

Note: This is a reference cited in *AP 42, Compilation of Air Pollutant Emission Factors, Volume I Stationary Point and Area Sources*. AP42 is located on the EPA web site at www.epa.gov/ttn/chief/ap42/

The file name refers to the reference number, the AP42 chapter and section. The file name "ref02_c01s02.pdf" would mean the reference is from AP42 chapter 1 section 2. The reference may be from a previous version of the section and no longer cited. The primary source should always be checked.

Los Gatos Tomato Products
Compliance
Emissions Testing
Test Dates: Feb 14, Mar 27,
Apr 11, 1991

BEST ENVIRONMENTAL, INC.

27343 Industrial Boulevard, Unit E.
Hayward, California 94545
(415) 784-0706

April 24, 1991

Los Gatos Tomato Products
P.O. Box 429
Huron, CA 93234

Attn: Mr. Dave Pompiano

Subject: Compliance Emissions Testing

Test Date: February 14, March 27, & April 11, 1991.

Sampling Location: Outlets of Boilers #1 & 2 at the Los Gatos Tomato Products facility near Huron, California.

Sampling Personnel: Regan Best, Sherman Smith and Dan Ashlin of BEST ENVIRONMENTAL.

Process Description: Los Gatos Tomato Products operates two Cleaver-Brooks boilers for steam production. The boilers are fired with natural gas and rated at 75,000 lbs/hr steam.

Test Program: Boiler emissions were continuously monitored for CO, O₂, CO₂, THC and NO_x concentration at the boiler outlets. Triplicate fourty minute test runs with calibrations before and after each run were performed on the boilers. Boiler #1 was tested on 2/14/91 and Boiler #2 on 3/27/91. Boiler #1 was retested on 4/11/91 due to high TNMHC levels found during the 2/14/91 test. Fuel rate data was recorded for each test. Volumetric flowrate measurements were taken at the boiler outlets. All tests were performed with the boilers on high fire.

Sampling Methods: The following Source Test Methods of the California Air Resouces Board (CARB) and the U.S. Environmental Protection Agency were used:

Method 1-100	CO ₂ , NO _x , O ₂ , CO, THC, Continuous Sampling
EPA Method 19	Emission Rate Determination using F-factor
EPA Method 1 & 2	Volumetric Flowrate Determination

Instrumentation:

Horiba Model PIR-2000 CO2 Analyzer

Infrared Ind. Model 2200 O2 Analyzer

Thermo Electron Model 10 NOx Analyzer

Thermo Electron Model 48 CO Analyzer

Bendix Model 8401 Total Hydrocarbon Analyzer

Test Results: Table 1 presents the results of the Boiler #1 emissions tests performed on 2/14/91. Average NOx concentration and NOx @ 3% O2 were 27.7 and 27.1 ppm, respectively. Average NOx emission factor and emission rate were 0.033 lbs/MMBtu and 2.90 lbs/hr. Average CO concentration and emission rate were 75.7 ppm and 4.84 lbs/hr. Average TNMHC concentration and emission rate were 24.0 ppm and 0.88 lbs/hr. Fuel rate was 1,408 SCFM. Boiler #1 failed to achieve the compliance standard of 15 ppm TNMHC 3% and 0.51 lbs/hr on this test day.

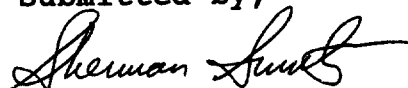
Table 2 presents the results of the Boiler #2 emissions tests performed on 3/27/91. Average NOx concentration and NOx @ 3% O2 were 26.2 and 26.1 ppm, respectively. Average NOx emission factor and emission rate were 0.032 lbs/MMBtu and 2.63 lbs/hr. Average CO concentration and emission rate were 94.4 ppm and 5.78 lbs/hr. Average TNMHC concentration and emission rate were 2.9 ppm and 0.10 lbs/hr. Fuel rate was 1,336 SCFM.

Table 3 presents the results of the Boiler #1 emissions tests performed on 4/11/91. Average NOx concentration and NOx @ 3% O2 were 28.1 and 27.5 ppm, respectively. Average NOx emission factor and emission rate were 0.033 lbs/MMBtu and 2.72 lbs/hr. Average CO concentration and emission rate were 79.8 ppm and 4.72 lbs/hr. Average TNMHC concentration and emission rate were 0.8 ppm and 0.0003 lbs/hr. Fuel rate was 1,311 SCFM.

Strip chart recordings, field data sheets and calibration gas certifications are contained in the appendix to this report.

If there are any questions concerning this report, please contact Regan Best at (415) 784-0708.

Submitted by,



Sherman Smith
Environmental Consultant

TABLE 1
Los Gatos Tomato Boiler No.1
TEST RESULTS

TEST	1	2	3	AVERAGE
TEST LOCATION	OUTLET	OUTLET	OUTLET	
TEST DATE	2-14-91	2-14-91	2-14-91	
TEST TIME	1538-1618	1642-1722	1725-1805	
FUEL RATE, SDCFM	1,408	1,408	1,408	1,408
MMBtu/hr	87.8	87.8	87.8	87.8
O2, %	2.6	2.7	2.6	2.6
CO2, %	10.4	10.4	10.4	10.40
NOx, ppm	28.00	28.00	27.00	27.67
NOx, ppm corr. 3% O2	27.39	27.54	26.41	27.1
NOx, Lbs/MMBtu	0.033	0.034	0.032	0.033
NOx, lbs/hr	2.93	2.94	2.82	2.90
CO, ppm	77.0	75.0	75.0	75.7
CO, Lbs/MMBtu	0.056	0.055	0.055	0.055
CO, lbs/hr	4.91	4.81	4.79	4.84
TNMTHC, ppm	25.0	27.0	20.0	24.0
TNMTHC, Lbs/MMBtu	0.0104	0.0113	0.0083	0.0100
TNMTHC, lbs/hr	0.91	0.99	0.73	0.88

Where,

CO = Carbon Monoxide
NOx = Oxides of Nitrogen
CO2 = Carbon Monoxide
TNMTHC = Total Non-Methane Hydrocarbons
MMBtu/hr = Million BTU per Hour Input
ppm = Parts Per Million Concentration
lbs/hr = Pounds Per Hour Emission Rate
lbs/MMBtu = Pounds per Million BTU Emission Factor

(See report
Table 3)

Calculations,

$$\text{lbs/MMBtu} = \text{ppm} \times 8740 \times 2.59 \times 10^{-9} \times \text{Mol. Wt.} \times (20.9/20.9-\text{O}_2)$$

$$\text{MMBtu/hr} = 1040 \text{ Btu/cf} \times \text{fuel SCFM} \times 60\text{min/hr} \times 10^{-6}$$

$$\text{lbs/hr} = \text{MMBtu/hr} \times \text{lbs/MMBtu}$$

$$\text{NOx corr. 3\% O}_2 = \text{NOx ppm} \times (17.9/20.9 - \text{O}_2)$$

TABLE 2
Los Gatos Tomato Boiler No.2
TEST RESULTS

TEST	1	2	3	AVERAGE
TEST LOCATION	OUTLET	OUTLET	OUTLET	
TEST DATE	3-27-91	3-27-91	3-27-91	
TEST TIME	1320-1400	1413-1453	1501-1541	
FUEL RATE, SDCFM	1,336	1,336	1,336	1,336
MMBtu/hr	82.8	82.8	82.8	82.8
O2, %	2.8	2.9	3.1	2.9
CO2, %	10.7	10.5	10.4	10.53
NOx, ppm	26.90	26.40	25.30	26.20
NOx, ppm corr. 3% O2	26.60	26.25	25.44	26.1
NOx, Lbs/MMBtu	0.032	0.032	0.031	0.032
NOx, lbs/hr	2.68	2.65	2.57	2.63
CO, ppm	114.5	92.5	76.3	94.4
CO, Lbs/MMBtu	0.084	0.068	0.057	0.070
CO, lbs/hr	6.97	5.66	4.72	5.78
THC, ppm	5.3	1.5	2.0	2.9
THC, Lbs/MMBtu	0.0022	0.0006	0.0009	0.0012
THC, lbs/hr	0.18	0.05	0.07	0.10

Where,

CO = Carbon Monoxide
NOx = Oxides of Nitrogen
CO2 = Carbon Monoxide
THC = Total Hydrocarbons
MMBtu/hr = Million BTU per Hour Input
ppm = Parts Per Million Concentration
lbs/hr = Pounds Per Hour Emission Rate
lbs/MMBtu = Pounds per Million BTU Emission Factor

Calculations,

$$\text{lbs/MMBtu} = \text{ppm} \times 8740 \times 2.59 \times 10^{-9} \times \text{Mol. Wt.} \times (20.9/20.9 - \text{O}_2)$$

$$\text{MMBtu/hr} = 1040 \text{ Btu/cf} \times \text{fuel SCFM} \times 60\text{min/hr} \times 10^{-6}$$

$$\text{lbs/hr} = \text{MMBtu/hr} \times \text{lbs/MMBtu}$$

$$\text{NOx corr. 3\% O}_2 = \text{NOx ppm} \times (17.9/20.9 - \text{O}_2)$$

TABLE 3
Los Gatos Tomato Boiler No.1
TEST RESULTS

TEST	1	2	3	AVERAGE
TEST LOCATION	OUTLET	OUTLET	OUTLET	
TEST DATE	4-11-91	4-11-91	4-11-91	
TEST TIME	1408-1448	1500-1540	1548-1628	
FUEL RATE, SDCFM	1,311	1,311	1,311	1,311
MMBtu/hr	81.3	81.3	81.3	81.3
O2, %	2.6	2.7	2.6	2.6
CO2, %	10.5	10.4	10.4	10.43
NOx, ppm	28.00	28.00	28.20	28.07
NOx, ppm corr. 3% O2	27.39	27.54	27.58	27.5
NOx, Lbs/MMBtu	0.033	0.034	0.034	0.033
NOx, lbs/hr	2.71	2.73	2.73	2.72
CO, ppm	80.7	80.0	78.8	79.8
CO, Lbs/MMBtu	0.059	0.058	0.057	0.058
CO, lbs/hr	4.77	4.75	4.66	4.72
THC, ppm	2.0	0.5	0.0	0.8
THC, Lbs/MMBtu	0.0008	0.0002	0.0000	0.0003
THC, lbs/hr	0.07	0.02	0.00	0.03

Where,

CO = Carbon Monoxide
NOx = Oxides of Nitrogen
CO2 = Carbon Monoxide
THC = Total Hydrocarbons
MMBtu/hr = Million BTU per Hour Input
ppm = Parts Per Million Concentration
lbs/hr = Pounds Per Hour Emission Rate
lbs/MMBtu = Pounds per Million BTU Emission Factor

Calculations,

$$\text{lbs/MMBtu} = \text{ppm} \times 8740 \times 2.59 \times 10^{-9} \times \text{Mol. Wt.} \times (20.9/20.9-\text{O}_2)$$

$$\text{MMBtu/hr} = 1040 \text{ Btu/cf} \times \text{fuel scfm} \times 60\text{min/hr} \times 10^{-6}$$

$$\text{lbs/hr} = \text{MMBtu/hr} \times \text{lbs/MMBtu}$$

$$\text{NOx corr. 3\% O}_2 = \text{NOx ppm} \times (17.9/20.9-\text{O}_2)$$

APPENDIX

CONTINUOUS MONITOR DATA SHEET

Plant Los Gatos Tomatoes

Date 2-14-91

Test Location Boiler #1

Run Number 1-2

Operator SS/DA

Ambient Temperature 65°F

Barometric Pressure 29.57

Static Pressure Quot

Fuel

Time	Sample Point	Fuel Flow	Dry Uncorrected					3% O ₂ Dry		Hydrocarbons			TOC ppm	CO ₂ ppm	VOC ppm	Comments
			O ₂ %	CO ₂ %	CO ppm	SO ₂ ppm	NO ppm	NO _x ppm	NO _x ppm	THC	CH ₄	Non CH ₄				
Run 2	1558	span	7.66	11.84	397			91.8		5592						
	1548	1	8.5	10.4	78			28		200	175	25				
	1558	2	8.7	10.3	75			28		200						
	1608	3	8.7	10.4	75			28		200						
	1618	4	8.5	10.4	80			28		200	175	25				
	1618	AVG	8.6	10.4	77			28		5303						
	1618	360	8	10	8			92		5400						
	1642	end	7.66	11.84	397			91.8		5592						
	1652	span	8.7	10.4	75			28		200						
	1702	2	8.7	10.4	73			28		210						
Run 3	1712	3	8.7	10.4	75			28		200						
	1722	AVG	8.5	10.4	75			28		200	175	27				sp Avg.
	1722	260	8.7	10.4	75			28		202						zero span
	1722	260	8	10	25			92		5600						
	1725	CAL	7.66	11.84	397			91.8		5592						
	1735	span	8.5	10.4	73			27		200	195					
	1745	1	8.5	10.4	78			28		210						
	1755	2	8.5	10.4	75			27		230						
	1805	3	8.6	10.4	75			27		220						
	1805	4	8.6	10.4	75			27		215	195	27				201
Run 4	1805	AVG	7.66	11.84	405			91.5		5600						
	1805	zero	8	10	2			91.5		5600						
	1805	CAL	7.66	11.84	405			91.5		5600						

1733
 1743
 1753

Run 2
 1702
 1716
 1738

Run 1
 1610
 1642

1738
 Boiler #1
 2-14-91
 1000-1000am
 1000-5000am



7403

761202

7402

7401

Barter #1
For Gabon Tomatoes
2-14-91

760202

O₂ 0-25%
CO₂ 0-15%

7403

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7403

Run 3
 1744
 1735
 1728

Run 2
 1735
 1728
 1721

Run 1
 1744
 1735
 1728
 1721

Reading is 1 on 6000 ppm range

Barber #1

Barber

90
 80
 70
 60
 50
 40
 30
 20
 10

CONTINUOUS MONITOR DATA SHEET

Ambient Temperature	~60
Barometric Pressure	29.65
Static Pressure Duct	
Fuel	Aut. Gas

Plant Las Batas Tomato
 Date 3-27-91
 Test Location Boiler 2
 Run Number 1, 2, 3
 Operator RB/DA

Time	Sample Point	Fuel Flow	Dry Uncorrected						3% O ₂ Dry		Hydrocarbons			TOC ppm	CO ₂ ppm	VOC ppm	Comments	
			O ₂ %	CO ₂ %	CO ppm	SO ₂ ppm	NO ppm	NO _x ppm	ppm	NO _x ppm	THC	CH ₄	Non CH ₄					
1300	On		7.0	12.2	410													Back check O.N.
1330	Start		27.5	10.7	120				27									
1340			27.7	10.7	125				27									
1350			27.8	10.7	125				27									
1400	End		27.8	10.7	108				27									Average Zero Span
1410			27.8	10.7	114.5				27									
1420			27.8	10.7	114.5				27									
1430			27.8	10.7	114.5				27									
1440	Start		27.8	10.5	100				26.5									Average Zero Span
1450			27.8	10.5	95				26.5									
1460			27.8	10.5	85				26.5									
1470			27.8	10.5	85				26.5									
1480	End		27.8	10.5	92.5				26.5									Average Zero Span
1490			27.8	10.5	92.5				26.5									
1500			27.8	10.5	92.5				26.5									
1510			27.8	10.5	92.5				26.5									
1520			27.8	10.5	92.5				26.5									Average Zero Span
1530			27.8	10.5	92.5				26.5									
1540			27.8	10.5	92.5				26.5									
1550			27.8	10.5	92.5				26.5									
1560	End		27.8	10.5	92.5				26.5									Average Zero Span
1570			27.8	10.5	92.5				26.5									
1580			27.8	10.5	92.5				26.5									
1590			27.8	10.5	92.5				26.5									
1600			27.8	10.5	92.5				26.5									Average Zero Span
1610			27.8	10.5	92.5				26.5									
1620			27.8	10.5	92.5				26.5									
1630			27.8	10.5	92.5				26.5									
1640	End		27.8	10.5	92.5				26.5									Average Zero Span
1650			27.8	10.5	92.5				26.5									
1660			27.8															

14403

14423

14411

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1443

14430

14411

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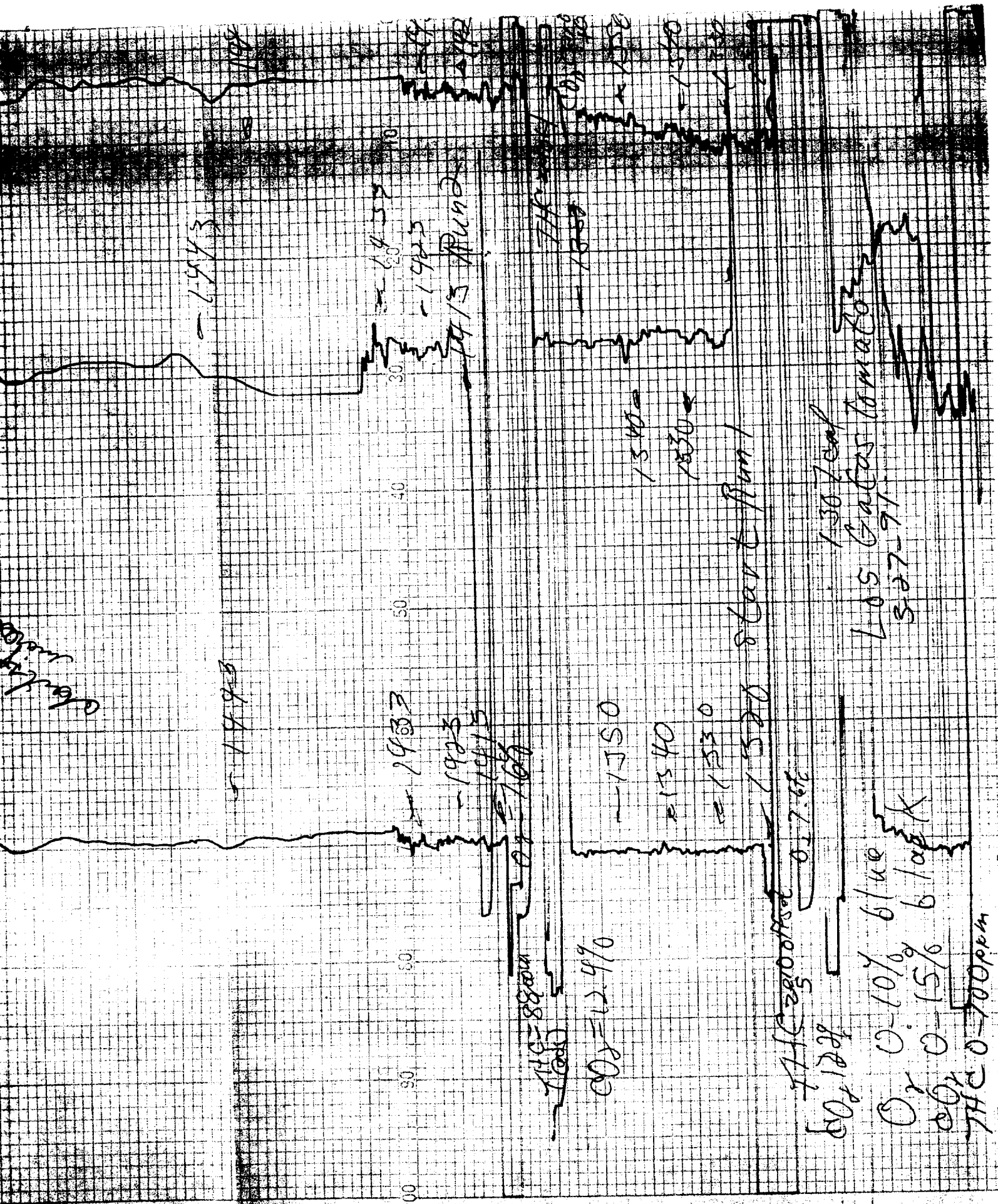
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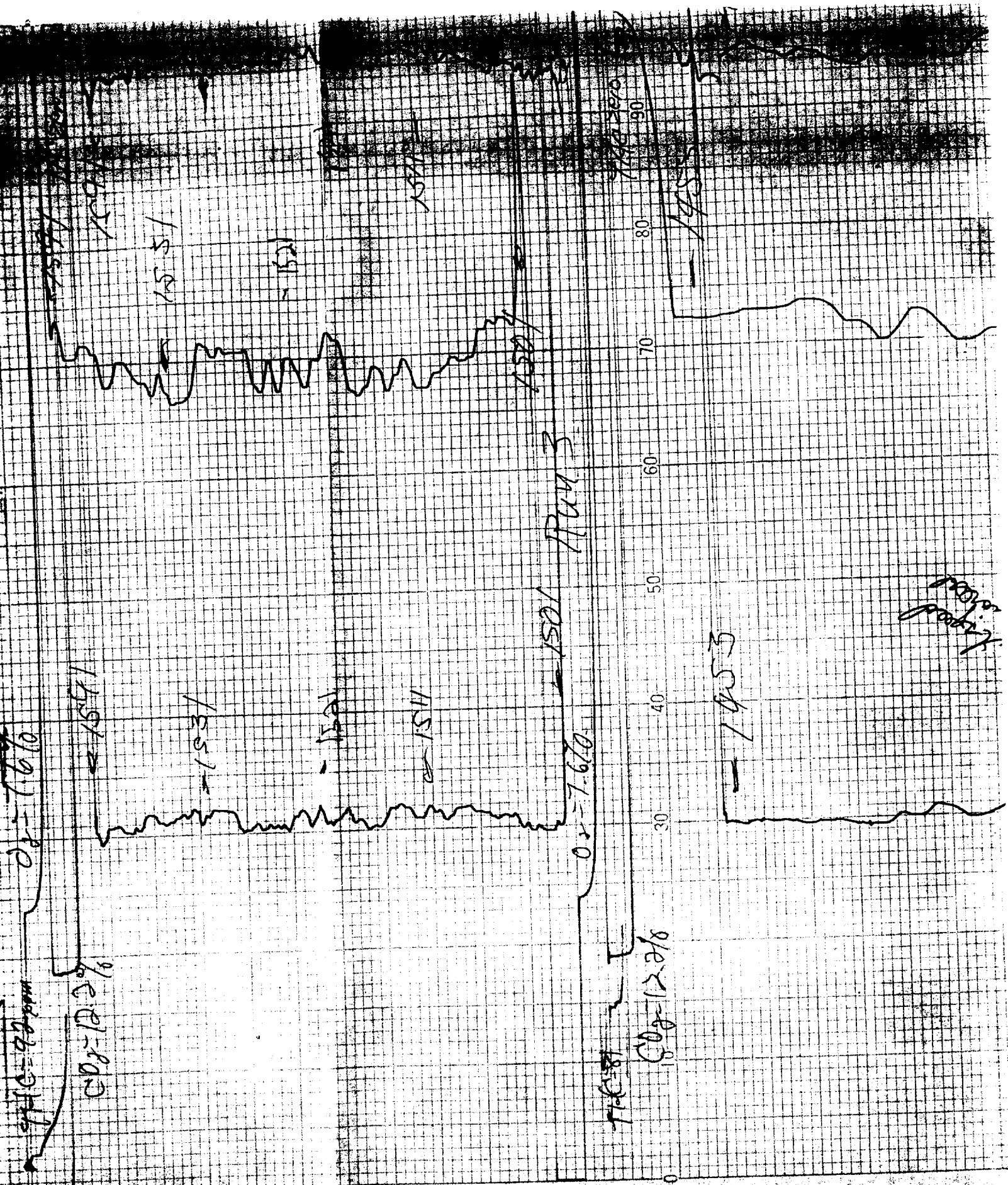
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STACK VOLUMETRIC FLOW RATE DETERMINATION

Stack gas velocity at stack conditions (ft/sec)

$$V_s = 85.49 (C_p) \left(\frac{.891}{\sqrt{\Delta P}} \right)_{avg} \sqrt{\frac{T_{s,avg} \cdot 460}{P_s MW_s}} = 61.4 \text{ ft/sec}$$

2.8% O₂
10.5% CO₂
16.8% H₂O

MW_s 27.88

Stack gas volume at standard conditions (scfm)

$$Q_s = 60 (1 - B_{wo}) V_{s,avg} A_s \left(\frac{528}{T_{s,avg} \cdot 460} \right) \left(\frac{P_s}{29.92} \right) = 14,946 \text{ scfm}$$

VELOCITY TRAVERSE DATA

Traverse Point Number	Velocity Head in. H ₂ O	Distance from Inside Wall (in.)	Stack Temperature (T _s) °F	Velocity Head in. H ₂ O	ΔP	Stack Temperature (T _s) °F
1	.70		305°		.837	
2	.72				.849	
3	.80				.874	
4	.95				.975	
5	.83				.911	
6	.60		290°		.775	
1	.82		305°		.906	
2	.84				.917	
3	.90				.979	
4	.89				.943	
5	.79				.889	
6	.72		295°		.849	
Average			299		.891	

Plant Los Gatos Tomato

Pitot Tube Factor 84

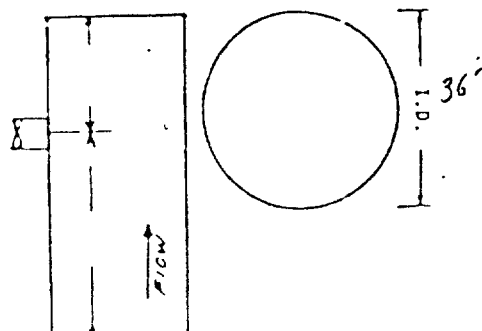
Sampling Site Unit #2 Boiler

Remarks _____

Barometric Pressure, in. Hg 29.65

Static Pressure in Stack (P_s) in. Hg + .13

Operators SS/DA Date 3/27/91



CONTINUOUS MONITOR DATA SHEET

Plant: Los Gatos Tomatoes

Date: 4/11/91

Test Location: Boiler #1

Run Number: 1, 2, 3

Operator: CT/SS

Ambient Temperature:

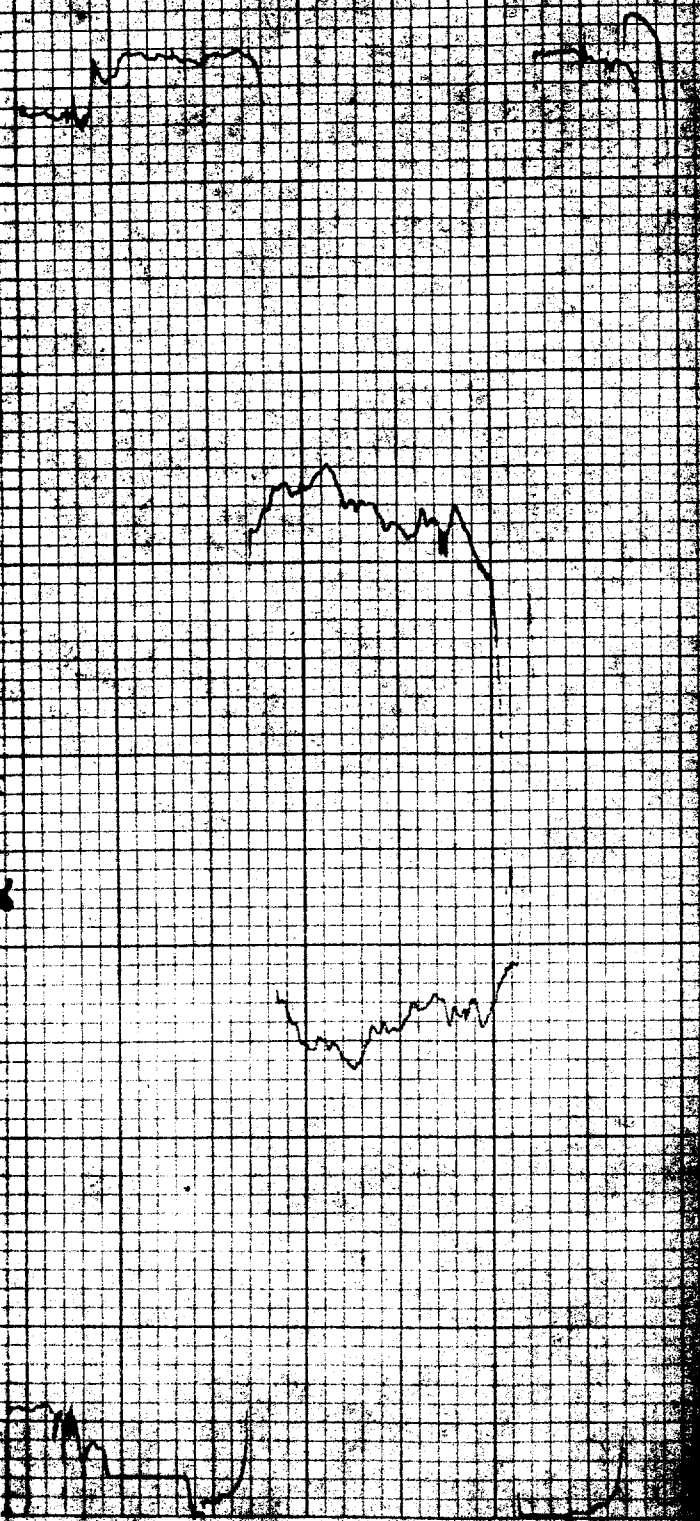
Barometric Pressure:

Static Pressure:

Fuel: Nat Gas

30.4

Time	Sample Point	Fuel Flow	Dry Uncorrected				32 O2 Dry		Hydrocarbons				Comments
			CO	CO2	CO	NO	NOx	ppm	ppm	THC	CH4	HC	
1408	cal/start		7.37	11.81	388		81.6			89.7			Run #1 55 scfm gas - 8.5 psi 100 = 10.8 / x 3600 = 14.2728 = 78.684 xh
1418			2.7	10.4	82.5		27.9			5.5	3.5	2.0	
1428			2.6	10.5	85		28		27.4	3.5			
1438			2.6	10.5	87		28			3.0			
1448			2.6	10.4	90		28			3.0			
1458			2.6	10.45	80		28			3.8	3.5	2.0	Run 2 1, 311 scfm gas
Ave			2.6	10.45	80		28			-2.0			
2000			2.4	11.88	40.5		80.9			89			
CAL													
1500	cal/start		7.37	11.81	388		81.6			89.7			
1510			2.7	10.4	80		28			5.5	4.5	1.5	Run 3
1520			2.6	10.4	80		28			5.0			
1530			2.6	10.4	80		28			4.8			
1540			2.7	10.4	80		28			4.7			
Ave			2.65	10.4	80		28			0			
2000			0	0	5		2			90			Run 3
CAL			7.3	11.8	382		82			89.7			
1548	cal/start		7.37	11.91	388		81.6			4.9			
1558			2.6	10.4	82.5		28			4.4	4.4	0	
1608			2.6	10.4	77.5		28			4.2			
1618			2.6	10.4	77.5		28.2			4.2	4.2	0	Run 3
1628			2.6	10.4	77.5		28.4			4.2	4.2	0	
Ave			2.6	10.4	78.8		28.3			4.4	4.4	0	
2000			0	0	10		4			0			
CAL			7.4	11.78	395		82.5			89.7			



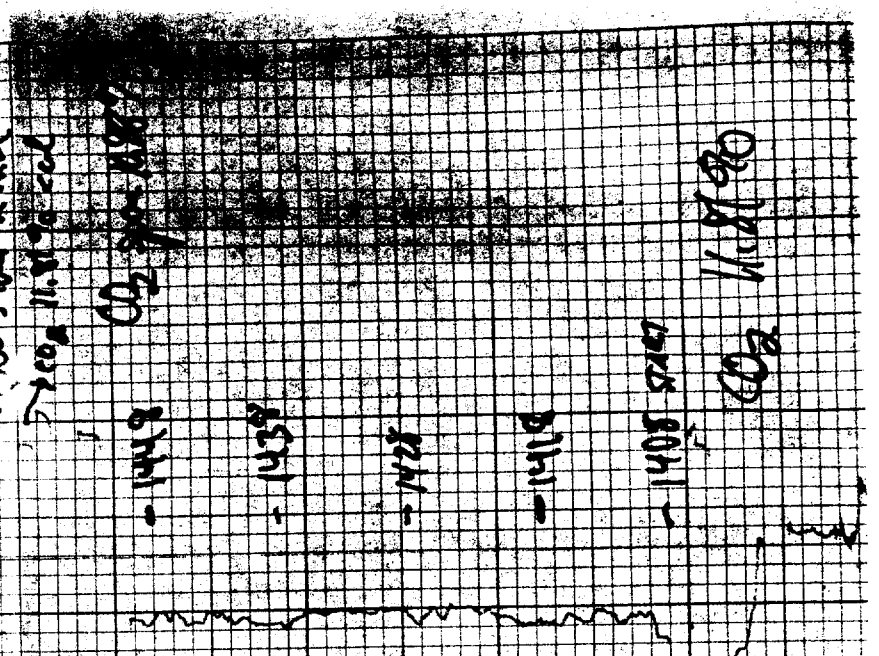
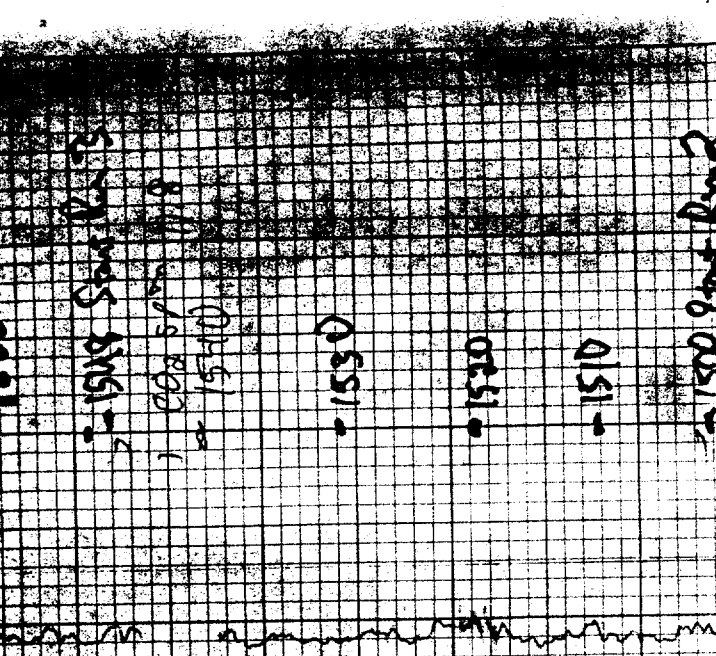
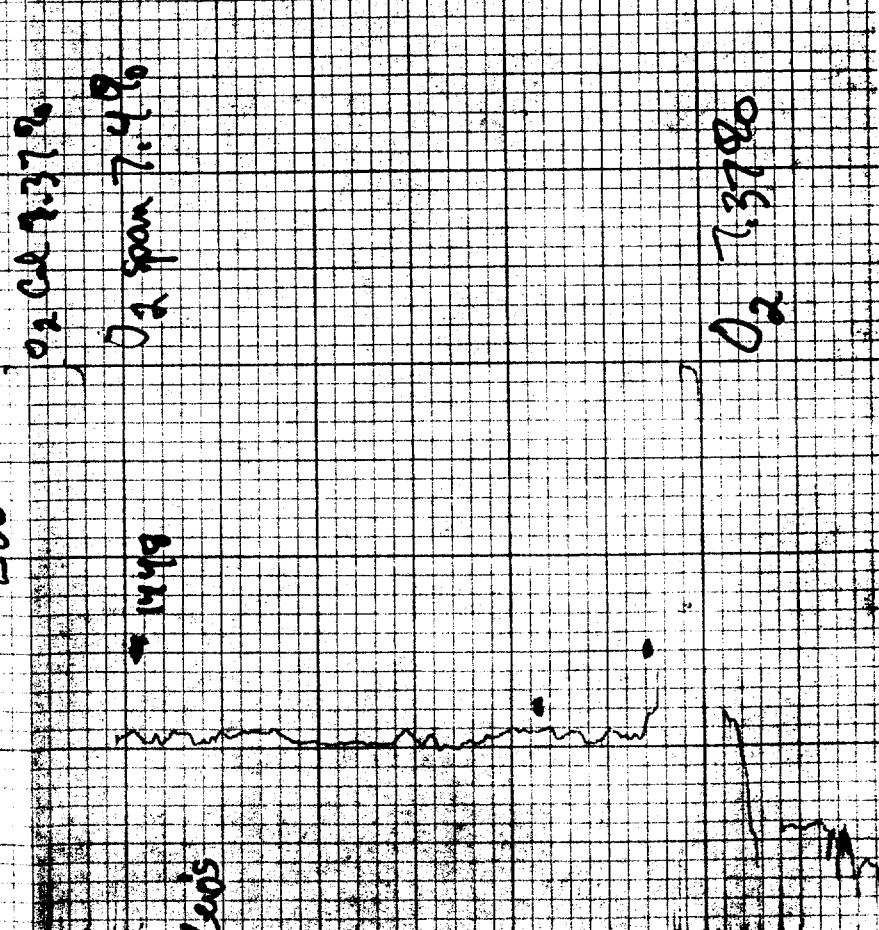
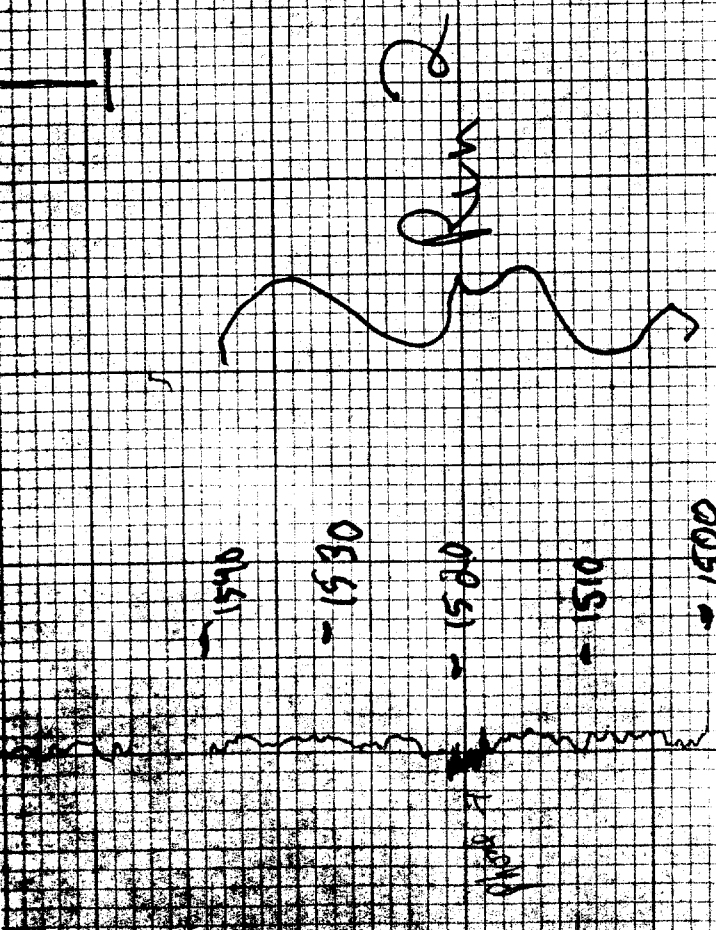
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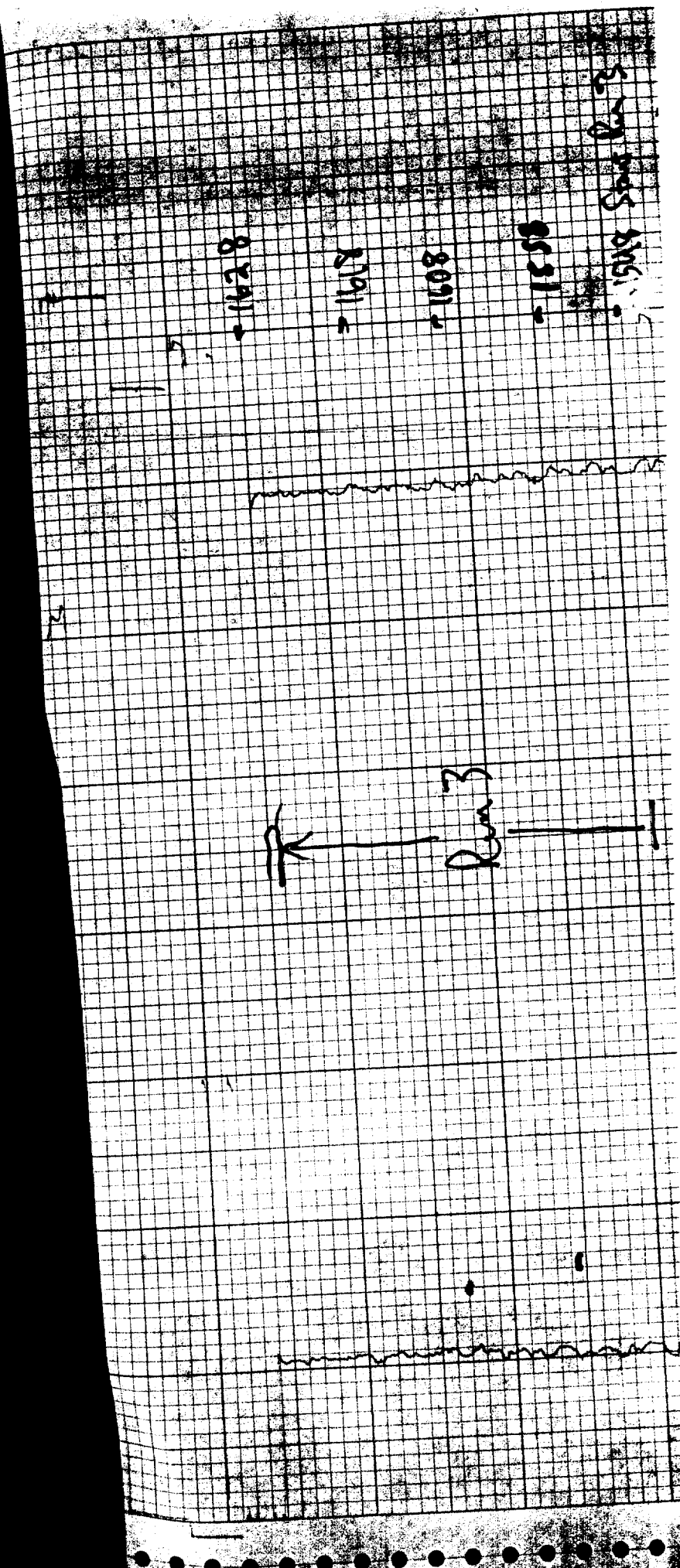
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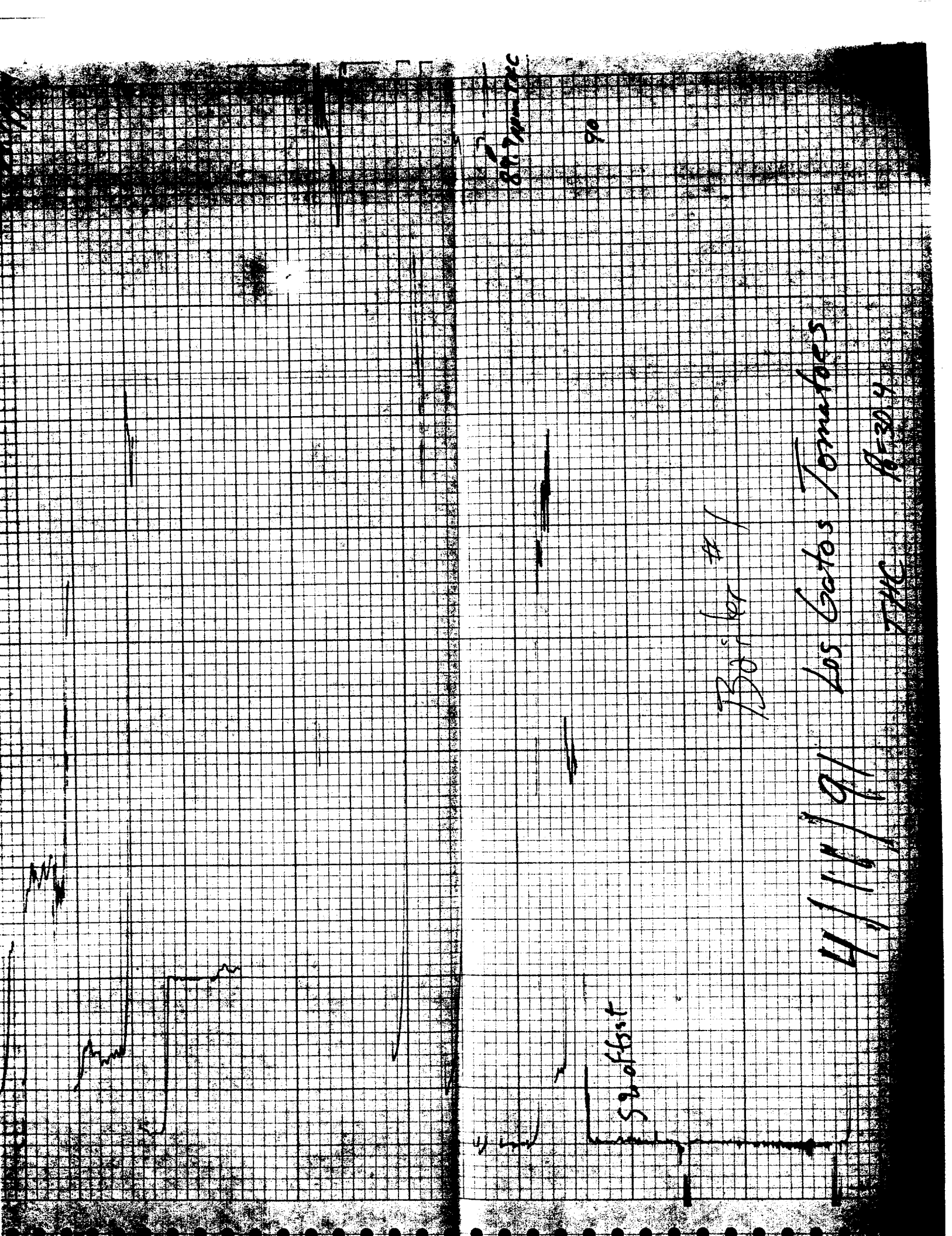
Boiler #1

4/11/91 Los Gatos Tomatoes

$P_0 = 30.4$ Red = O_2 0-25%
 Blue = CO_2 0-25%







500 ft

300 ft

Los Gatos Tomatoes

4/11/91

JHC

8/30/91

8/30/91

90

Start Run 3

1548

1540

1530

1520

1510

Start Run 2

1500

Run 2

Run 1518

Run 1518

1448

1438

1428

1418

1408

Run 1

CHC

CHY

1408 Start

1408 Start

CHC

CHY

1408 Start

1408 Start

1408 Start

1408 Start

1408 Start

1408 Start

1408 Start

1628

1619

1608

1558

Run 3

3044

2443

STACK VOLUMETRIC FLOWRATE DETERMINATION

Date 4/11/91 client Los Gatos Tomato Operators SS/DA
Time _____ Barometric (Pb) _____ Static _____
Location Boiler / Duct Pressure _____ Pressure +0.21
Pitot Factor .84 Duct dimen. 36" ID. _____
CO2% 10.4 Stack Area (As) 7.07
O2% 2.6 Round duct = $\pi r^2 \div 144$ (radius in inches)
H2O% _____

Velocity Traverse Data

Remarks

Inches from wall	Port &pt.	Time	Delta P	Stack Temp	sqr.t. °P
1.0	1		.70	302	.837
2.4	2		.70	300	.837
4.25	3		.70	300	.837
6.37	4		.71	299	.843
9.0	5		.76	298	.872
12.8	6		.78	300	.883
23.2	7		.90	296	.949
27.0	8		.88	298	.938
29.6	9		.80	298	.895
31.75	10		.78	298	.883
33.6	11		.60	296	.775
35.0	12		.60	296	.775
	1		.70	306	.837
	2		.68	305	.825
	3		.75	303	.866
	4		.80	300	.894
	5		.85	299	.922
	6		.83	302	.911
	7		.88	298	.938
	8		.87	297	.933
	9		.80	295	.895
	10		.81	297	.900
	11		.81	295	.900
	12		.79	295	.889
Averages				298.9	.874

Stack Gas Velocity
@ Stack conditions
(feet per second)

$$V_s = 85.49 \times (C_p) \times \sqrt{p_{avg} \times \sqrt{[Ts_{avg} \times 460 / Ps_{MWs}]}}$$

Where,

Vs=velocity stack

$C_p = \text{pitot factor}$

Ts=Stack Temperature

Ps=Stack pressure

MWs=Molecular Wt.gas

where,

$$MWS = MWd \times (1 - Bwo) + 18 (Bwo)$$

$$\text{MWd} = .44 (\% \text{CO}_2) + .32 (\% \text{O}_2) + .28 (\% \text{CO} + \% \text{N}_2)$$

$$B_{wo} = \% \text{moisture} / 100$$

$$P_s = \text{static} / 13.6 + P_b$$

Stack Gas Volume at
Standard Conditions

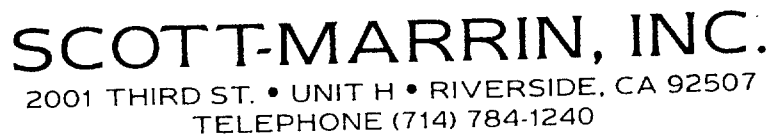
$$Q_S = \text{SCFM}$$

$$Q_s = 60(1 - B_{wo}) \times V_{savg} \times A_s \times (528 / T_{savg} + 460) \times (P_s / 29.92)$$

$V_S =$ _____

QS= 14,860

Notes/Comments



BEST01

TO:

DAN CARTNER
BEST ENVIRONMENTAL
27343 INDUSTRIAL BLVD.
HAYWARD, CA 94545

DATE : 08/02/90

CUSTOMER ORDER NUMBER: 8168

PAGE 1

COMPONENT	CONCENTRATION (v/v)	REFERENCE STANDARD	ANALYZER MAKE, MODEL, S/N, DETECTION	EXPIRATION DATE	REPLICATE ANALYSIS DATA	
CYLINDER NO.:	CC42792					
Nitric Oxide	91.8 ± 0.9 ppm	GMIS	Monitor Labs Model 8440 S/N 136	01/24/92	07/17/90 92.0 ppm	07/24/90 91.6 ppm
		Cylinder #	Continuous		91.8 ppm	91.5 ppm
Nitrogen, O ₂ -Free Balance		CC83831	Chemiluminescence		91.9 ppm	91.8 ppm
Cylinder Pressure: 2000 psig		@ 101.8 ppm	Last Cal Date: 07/30/90	Mean:	91.9 ppm	91.6 ppm

$$\text{ppm} = \text{umole/mole}$$
$$\% = \text{mole-}\%$$

The above analyses were performed in accordance with EPA-1987 Traceability Protocol # 1, Section 3.0.4, Procedure G1.

Analyst:

J.W. Gay

Approved:

J.T.Marrin

The only liability of this company for gas which fails to comply with this analysis shall be replacement or reanalysis thereof by the company without extra cost.

STANDARD CALIBRATION GASES IN ALUMINUM CYLINDERS



BEST01

TO:

DAN CARTNER
BEST ENVIRONMENTAL
27343 INDUSTRIAL BLVD. #E
HAYWARD, CA 9454

CUSTOMER ORDER NUMBER: 8205

PAGE 1

ppm = umole/mole % = mole-%

The above analyses were performed in accordance with EPA-1987 Traceability Protocol # 1, Section 3.0.4, Procedure G1.

Analyst: Steve Kozy
S.B. Kozy

Approved: J.T. Marrin
J.T. Marrin

The only liability of this company for gas which fails to comply with this analysis shall be replacement or reanalysis thereof by the company without extra cost.

STANDARD CALIBRATION GASES IN ALUMINUM CYLINDERS



2001 THIRD ST. • UNIT H • RIVERSIDE, CA 92507
TELEPHONE (714) 784-1240

REPORT OF ANALYSIS CALIBRATION GAS MIXTURES

BEST01

TO:

DATE : 03/05/91

REGAN BEST
BEST ENVIRONMENTAL
27343 INDUSTRIAL BLVD. #E
HAYWARD, CA 94545

CUSTOMER ORDER NUMBER: 8250

PAGE 1

CYLINDER NO.: CC60374

CYLINDER NO.: CC62457

COMPONENT	CONCENTRATION (v/v)
-----	-----
Propane	19.80 + 0.40 ppm
Methane	30.3 + 0.6 ppm
Air	Balance

COMPONENT	CONCENTRATION (v/v)
-----	-----
Carbon Dioxide	11.81 $\pm$ 0.24 %
Oxygen	7.37 $\pm$ 0.15 %
Carbon Monoxide	388 $\pm$ 8 ppm
Nitrogen	Balance

$$\text{ppm} = \text{umole/mole}$$

% = mole-%

Analyst:

Mark Pearson

M.J. Monson

Approved:

W. W. W.

J.T.Marrin

REPORT OF ANALYSIS
EPA PROTOCOL GAS MIXTURES

BEST01

TO:

DAN CARTNER
BEST ENVIRONMENTAL
27343 INDUSTRIAL BLVD., E
HAYWARD, CA 94545

DATE : 10/05/90

CUSTOMER ORDER NUMBER: 8205

PAGE 1

COMPONENT	CONCENTRATION (v/v)	REFERENCE STANDARD	ANALYZER MAKE, MODEL, S/N, DETECTION	EXPIRATION DATE	REPLICATE ANALYSIS DATA	
CYLINDER NO.:	CC62120					
Carbon Monoxide	397 $\pm$ 4 ppm	GMIS	Carle Insts Model 8800 S/N 8249	04/04/91	09/27/90	10/04/90
		Cylinder #	Methanation/FID		399 ppm	398 ppm
		CC28362	Gas Chromatography		397 ppm	393 ppm
		@ 495 ppm	Last Cal Date: 09/11/90		398 ppm	393 ppm
				Mean:	398 ppm	395 ppm
Carbon Dioxide	11.84 $\pm$ 0.12 %	GMIS	Varian Model 1860 S/N None	03/26/91	09/26/90	
		Cylinder #	Thermal Conductivity		11.82 %	
		CC60263	Gas Chromatography		11.83 %	
		@ 17.62 %	Last Cal Date: 07/19/90		11.86 %	
				Mean:	11.84 %	
Oxygen	7.66 $\pm$ 0.08 %	GMIS	Varian Model 1860 S/N None	03/24/91	09/24/90	
		Cylinder #	Thermal Conductivity		7.65 %	
Nitrogen	Balance	CC62350	Gas Chromatography		7.65 %	
Cylinder Pressure:	2000 psig	@ 9.68 %	Last Cal Date: 07/25/90		7.68 %	
				Mean:	7.66 %	

$$\text{ppm} = \text{umole/mole}$$

% = mole-%

The above analyses were performed in accordance with EPA-1987 Traceability Protocol # 1, Section 3.0.4, Procedure G1.

Analyst:

J.W. Gay

Approved:

J.T.Marrin

The only liability of this company for gas which fails to comply with this analysis shall be replacement or reanalysis thereof by the company without extra cost.

STANDARD CALIBRATION GASES IN ALUMINUM CYLINDERS



BEST01

DATE : 01/24/91

TO:

REGAN BEST
BEST ENVIRONMENTAL
27343 INDUSTRIAL BLVD., #E
HAYWARD, CA 94545

PAGE 1

CUSTOMER ORDER NUMBER: 8236

CYLINDER NO.: CC28068

CYLINDER NO.:

COMPONENT	CONCENTRATION (v/v)
Oxygen	7.58 ± 0.15 %
Carbon Dioxide	12.22 ± 0.24 %
Carbon Monoxide	410 ± 8 ppm
Nitrogen	Balance

COMPONENT	CONCENTRATION (v/v)
-----	-----

$$\text{ppm} = \text{umole/mole}$$

% = mole-%

Analyst: Mark Monson
M.J. Monson

Approved:

J.T.Marrin

The only liability of this company for gas which fails to comply with this analysis shall be replacement or reanalysis thereof by the company without extra cost.

STANDARD CALIBRATION GASES IN ALUMINUM CYLINDERS