

ENVIROTECH



EBSP

P.O. Box 96

Belmont, California 94002

Telephone (415) 593-1021

Telex 348360

STAPPA/ALAPCO

2.5

logged 1/28/86

#06

16

This Report was Reviewed

by: JusDate: 10/8/83

and found to be

Satisfactory: ☒Unsatisfactory: ☐Remarks: See Memo

incomplete

PERFORMANCE TEST REPORT

ROCKY MOUNT

WASTEWATER TREATMENT FACILITY

MHF SLUDGE INCINERATOR

☐ APPROVED	☒ APPROVED AS NOTED
☐ NOT APPROVED - RESUBMIT	☐ SEE LETTER
For Use on <u>0081-B1</u>	
For general compliance with plans & specifications.	
Contractor to check and verify quantities, dimensions, etc.	
PEIRSON & WHITMAN, INC.	
By <u>PEL</u>	Date <u>5-6-83</u>
☐ P & W Copy	☐ Insp't'r Copy
☐ City Copy	
LOG ITEM # <u>242</u>	IN LOG # <u>5954</u>
SPEC. SECT. <u>1020</u>	

W.E. Nance
D.E.M. ~~W.E. Nance~~
D.A.Q.

☐ APPROVED	☐ APPROVED AS NOTED
☒ NOT APPROVED - RESUBMIT	☒ SEE LETTER
For Use on <u>0081-B1</u>	
For general compliance with plans & specifications.	
Contractor to check and verify quantities, dimensions, etc.	
PEIRSON & WHITMAN, INC.	
By <u>PEL</u>	Date <u>4-7-85</u>
☒ P & W Copy	☐ Insp't'r Copy
☐ City Copy	
LOG ITEM # <u>242</u>	IN LOG # <u>5954</u>
SPEC. SECT. <u>1020</u>	

~~OFFICE COPY~~

DIVISION OF ENVIRONMENTAL MANAGEMENT
Air Quality Section

June 21, 1983

M E M O R A N D U M

TO: Robert Van Tilburg

ATTN: Ernie Fuller

FROM: Jule Shanklin

SUBJECT: SOURCE TEST REPORT REVIEW (Revised Memo)
Rocky Mount Wastewater Treatment Facility
SLUDGE INCINERATOR
Rocky Mount (Edgecombe County)

REF: (A) 40 CFR 60, Subpart O; Standards of Performance for Sewage
Treatment Plants
(B) 40 CFR 61, Subparts C & E; National Emission Standards for
Beryllium and Mercury (NESHAPS)
(C) NCAC 2D .0501; "Compliance with Emission Standards; section
(D) (3)"
(D) NCAC 2D .0505; "Control of Particulates from Refuse Burning"
(E) My memo, same subject, dated June 10, 1983

My previous memo on this subject cited the wrong NSPS standard. The applicable standard is Subpart O as cited above as Reference A. The particulate emission limit is 1.3 lb/ton of sludge charged and the summary has been rewritten to reflect this limit. Please mark-up the previous (Ref. E) memo and attach this memo to it.

The subject report for the 1/13/83 test performed by Envirotech/TRW has been reviewed and found acceptable to the extent of testing performed. This report covers only particulate testing concerned with our incinerator standard (Ref. D). However, NESHAPS for Mercury and Beryllium (Ref. B) as well as NSPS for Particulate (Ref. A) also apply to this source. There were no Hg or Be results.

We reserve the right to require that "back-half" extractions be included in certain Method 5 test results as explained in Ref. C. This was not done in the subject test. Because of the type source involved, I would recommend that in subsequent particulate tests we require a stipulation for back-half extractions.

Mr. Robert Van Tilburg
page 2
June 21, 1983

Results are summarized as follows:

<u>Emissions</u>	<u>Run 2</u>	<u>Run 3</u>	<u>Run 5</u>	<u>Avg.</u>
Particulate*				
lb/hr	0.652	0.525	0.459	0.545
Particulate*				
gr/dscf @ 12% CO ₂	.0474	.0340	.03177	.0377
Mercury	Not Meas.	Not Meas.	Not Meas.	—
Beryllium	Not Meas.	Not Meas.	Not Meas.	—
<u>Charge Rates</u>				
lb/hr	3946	4419	3997	—
<u>Limits</u>				
Part. (.0505)				
lb/hr	7.892	8.838	7.994	8.24
Part. (NSPS)				
lb/hr (based on 1.3 lb/ton limit)	2.56	2.87	2.60	2.67

*Based on front-half only

/la

cc: Dennis Ramsey
Walt Nance

DIVISION OF ENVIRONMENTAL MANAGEMENT
Air Quality Section

June 10, 1985

M E M O R A N D U M

TO: Robert Van Tilburg
ATTN: Ernie Fuller
FROM: Jule Shanklin *Jes*
SUBJECT: SOURCE TEST REPORT REVIEW
Rocky Mount Wastewater Treatment Facility
SLUDGE INCINERATOR
Rocky Mount (Edgecombe County)

*should be Subp. C
sewage sludge*

REF: (A) 40 CFR 60, Subpart E; Standards of Performance for Incinerators (NSPS)
(B) 40 CFR 61, Subparts C & E; National Emission Standards for Beryllium and Mercury (NESHAPS)
(C) NCAC 2D .0501; "Compliance with Emission Standards; section (D)(3)"
(D) NCAC 2D .0505; "Control of Particulates from Refuse Burning"

The subject report for the 1/13/83 test performed by Envirotech/TRW has been reviewed and found acceptable to the extent of testing performed. This report covers only particulate testing concerned with our incinerator standard (Ref. D). However, NESHAPS for Mercury and Beryllium (Ref. B) as well as NSPS for Particulate (Ref. A) also apply to this source. Using results and data in the report, I have calculated the emission concentrations at 12% CO₂, relative to NSPS limits, and included them in the test summary below. There were no Hg or Be results.

Also, we reserve the right to require that "back-half" extractions be included in certain Method 5 test results as explained in Ref. C. This was not done in the subject test. Because of the type source involved, I would recommend that in subsequent particulate tests we require a stipulation for back-half extractions.

Results are summarized as follows:

<u>Emissions</u>	<u>Run 2</u>	<u>Run 3</u>	<u>Run 5</u>	<u>Avg.</u>
Particulate*				
lb/hr	0.652	0.525	0.459	0.545
Particulate*				
gr/dscf @ 12% CO ₂	0.0474	0.0340	0.0318	0.0377
Mercury	Not Meas.	Not Meas.	Not Meas.	—
Beryllium	Not Meas.	Not Meas.	Not Meas.	—
Charge Rates				
lb/hr	3946	4419	3997	—

Mr. Robert Van Tilburg
page 2
June 10, 1983

<u>Emissions</u>	<u>Run 2</u>	<u>Run 3</u>	<u>Run 5</u>	<u>Avg.</u>
Limits				
Part. (.0505) lb/hr	7.892	8.838	7.994	8.24
Part. (NSPS) gr/dscf @ 13% CO ₂	0.08	0.08	0.08	—
Mercury (NESHAPS) lb/hr (based on 3200 g/24 hr)	0.294	0.294	0.294	—
Beryllium (NESHAPS) lb/hr (based on 10 g/24 hr)	.00092	0.00092	0.00092	—

* Based on front-half only

/la

cc: Dennis Ramsey

Calculation Summary

SOURCE ROCKY MOUNT/SLUDGE INCIN Date 1/13/83
 LOCATION Rocky Mount

ENTRY	RUN 2	RUN 3	RUN 5	ANSWER
Ave. ΔH (in H_2O)	2.9750	3.1420	3.3170	
P_{atm} (in Hg)	30.2000	30.2000	30.2000	
P_s (gage) (in H_2O)	30.4188	30.4310	30.4807	P_m (in Hg)
	-0.2200	-0.2200	-0.2200	
	30.1838	30.1838	30.1838	P_s (in Hg)
T_m ($^{\circ}R$)	534.0000	534.0000	529.0000	
V_m (ft ³)	53.3230	55.0000	60.4900	
	53.7939	55.5081	61.7264	V_{mstd} (ft ³)
V_{lq} (ml)	71.5000	38.0000	64.0000	
	3.3820	1.7974	3.0272	V_{vstd} (ft ³)
	57.1759	57.3055	64.7536	V_{std} (ft ³)
	5.9150	3.1365	4.6750	ZM
	0.9409	0.9686	0.9533	M_d
MW_d	29.4200	29.4500	29.3700	
	28.7445	29.0909	28.8385	M
T_s ($^{\circ}R$)	559.0000	558.6000	560.0000	
$\Sigma \sqrt{\Delta p}$	6.5902	6.8024	7.5099	
$n_{\Delta p}$	12.0000	12.0000	12.0000	Ave $\sqrt{\Delta p}$
C_p	0.5492	0.5669	0.6258	
	0.8400	0.8400	0.8400	v_s (ft/sec)
D_s (in)	31.6521	32.4646	36.0427	
	20.5000	20.5000	20.5000	A_s (ft ²)
	2.2921	2.2921	2.2921	Q_s (ft ³ /min)
	4353.	4465.	4957.	Q_{std} (ft ³ /min)
	4163.	4273.	4732.	
W_t (gm)	0.0676	0.0534	0.0470	pmr_c (lb/hr)
	0.6511	0.5267	0.4544	
D_n (in)	0.3100	0.3100	0.3100	A_n (in ²)
	0.0755	0.0755	0.0755	
θ (min)	60.0000	60.0000	60.0000	pmr_a (lb/hr)
	0.6518	0.5149	0.4532	ZI
	100.1097	97.7556	99.2443	pmr_{avg} (lb/hr)
	0.6515	0.5208	0.4538	
ZCO				
ZO_2				
ZN_2				
F Factor				ZEA
				HI (10 ⁶ BTU/hr)
				pmr_u (lbs/10 ⁶ BTU)

ENVIROTECH



EBSP

P.O. Box 98
Belmont, California 94002
Telephone (415) 593-1021
Telex 348360

PERFORMANCE TEST REPORT

ESBP CONTRACT NO. 5073-11

ONE 16' 9" O.D. X 6 HEARTH MULTIPLE HEARTH

SLUDGE INCINERATOR

ROCKY MOUNT WASTEWATER TREATMENT FACILITY

THE CITY OF ROCKY MOUNT, NORTH CAROLINA

CONSULTING ENGINEER

PEIRSON & WHITMAN INC.

GENERAL CONTRACTOR

WRENN-WILSON CONSTRUCTION CO.

TEST DIRECTION & REPORT BY:

G. F. KRONEBERGER, PRINCIPAL PROCESS ENGINEER, LURGI CORP., BELMONT, CA.

REPORT APPROVAL & SUBMITTAL BY:

H. L. LANGE, REGIONAL MANAGER, EBSP-ENVIROTECH, BATON ROUGE, LA.

FEBRUARY 24, 1983

TABLE OF CONTENTS

- I INTRODUCTION
- II SUMMARY AND CONCLUSIONS
- III DISCUSSION OF RESULTS
- IV TEST OPERATION, PROCEDURES, SAMPLING
& ANALYSES
- V APPENDAGE: TRW REPORT COMPLETE WITH
APPENDICES A THROUGH G

I. INTRODUCTION

Performance tests to demonstrate compliance with the EPA air pollution code CFR 40 and the specification requirements were conducted on the ESBP multiple hearth furnace at the Rocky Mount Wastewater Treatment Facility.

On January 13, 1982, this furnace demonstrated compliance with the specifications and applicable EPA requirements.

Present during the tests, either full or part time were:

City of Rocky Mount

F. E. Beaudry
Stanley Curtis
R. Casper and participating
laboratory personnel

North Carolina Department of Natural Resources

C. E. Fuller

Peirson & Whitman Inc.

H. M. Nance
Don Raynor

Wrenn-Wilson Construction Co.

O. Z. Wrenn
Ralph Whitfield
Roger McIntyre

EBSP/Envirotech

Hal Lange	Charlie Grace
Pat Owre	George Tabor

Independent Test Lab: TRW

Jim McReynolds	Dave Savia
----------------	------------

Lurgi Corporation

G. F. Kroneberger

The following section summarizes applicable test results.

II. SUMMARY AND CONCLUSIONS

The plant stored sludge for a period to accumulate sufficient sludge for the emission tests. As established in pre-test meetings the week of the test, the furnace was to be operated within the constraints of normal current operations. The furnace operated well and has adapted to the current mode of operation. The main operational change from the specifications are that less ash is recycled to the dewatering system. This results in a reduction of total dry solids for a corresponding quantity of sludge solids and a higher moisture percentage. The furnace handles the material well and it is assumed that this mode of operation is beneficial to the plant from an overall point of view.

The following section summarizes pertinent test results in the sequence occasioned by the specifications.

Operating Performance Test (Spec. 1Q 20.30)

The furnace was proved operational during 1982.

Feed Characteristics (Spec. 1Q 20.31) and Basis of Design and Testing (Spec. 1Q 20.37)

			<u>Actual</u>	
	<u>Design</u>	<u>Specified Variation</u>	<u>Field Weight Basis</u>	<u>Weight Corrected By Analysis</u>
Moisture content (% w.b.)	60%	60 to 65	64 to 70	67.7
Lbs. of dry sludge solids per hr	2320	1508 to 2320	1500 to 1908	1332
Lbs. of wet sludge cake per hr	5800	3770 to 5800	5000 to 5300	4124
Dry sludge combustibles as percent of d.s.	40	40 to 50	59 to 60	60
*Lbs. of volatile solids/hr.	928	527 to 928	985 to 1081	798
Wet feed based on new parameters	4686	2661 to 4686	---	4124
Calorific value of sludge (BTU/lb. of combustibles)	10,000	8,000 to 10,000	10,366 to 10,600	10,500

* Disposal Criteria

Basis of Design & Testing (Spec. IQ 20.37)

Pre-test meetings established that, in view of the proven past operation, the test period would be that required for the emission test.

1. No objectional odors were encountered.
2. Observation of the emission per standard procedures, indicated emissions were near Ringleman 0. Observations would be classified as marginally visible, with average opacity less than 9 percent.
3. Analytical Results of Particulate Samples:

The prime criteria for emission compliance is a particulate emission not exceeding 1.3 pounds per ton of dry solids fed to the furnace.

Test results for the three valid* tests are as follows:

<u>Test</u>	<u>Emission Particulates (Pounds/hr)</u>	<u>Based on Field Feed Weight (lbs/dry ton)</u>	<u>Based on corrected calculated feed weight ** (lbs/dry ton)</u>
No. 2	0.652	0.79	1.00
No. 3	0.525	0.62	0.74
No. 5	0.459	0.54	0.72

* Tests 1 & 4 were invalidated due to sampling problems.

** The corrected feed weight basis is an accurate weight which corrects for a calibration anomaly and which has been verified by an analytical carbon balance calculation the field calibration figures were corrected for hold-up in the conveyor system when changing rates. See Appendix sheets G-1, G-2 and G-3 for graphic presentations.

Test Conditions

Operation of the furnace during the tests was steady and the furnace was fed within the capabilities of the feed system and filter. Moisture levels ranged from 66 to 70% with an average of 68% during the test periods. Under these conditions the furnace operated properly and reduced the wet sludge to a sterile ash.

SUMMARY OF PARTICULATE MATTER EMISSION TEST RESULTS:

Test	Run #2	Run #3	Run #5
Date	1-13-83	1-13-83	1-13-83
Time	1105-1207	1235-1337	1537-1610
Sample Duration (min)	60	60	60
Sample Volume (DSCF)	53.562	55.268	60.601
Stack Flow (DSCFM)	3,916	4,120	4,488
Stack Temperature (°F)	98.8	98.6	99.9
Moisture (%)	5.9	3.1	4.7
CO ₂ (%)	4.92	5.25	4.51
O ₂ (%)	15.89	15.36	16.27
Excess Air (%)	317	274	350
Isokinetic (%)	98.9	97.0	97.6
Particulate Matter (lb/hr)	0.652	0.525	0.459
Feed Cakes Dry Solids (%)	33	32	32

SUMMARY OF PARTICULATE MATTER EMISSION TEST RESULTS:
(Continued)

Test		Run #2	Run #3	Run #5
*1	Wet Feed Rate (lb/hr)	5,000	5,300	5,300
	Dry Feed Rate (ton/hr)	0.82	0.85	0.85
	Emission Rate	0.79	0.62	0.54
*2	Wet Feed Rate (lb/hr)	3946	4419	3997
	Dry Feed Rate (ton/hr)	0.652	0.71	0.64
	Emission Rate	1.00	0.74	0.72
Visible Emissions (% Opacity)		6.6	9.0	8.9

*1 Based on preliminary field weight information

*2 Based on corrected weight checked with analysis calculation.

Furnace Feed (Spec. 1Q 20.37E.)

By design, the feed did not exceed the maximum specified rate. The system has a new maximum feed rate based on current operation. Using the original disposal requirements of dry sludge solids, new rates were developed based on current cake compositions. These were listed in the table at the beginning of this section. Key items are listed below:

	<u>Original Specification</u>	<u>Current Operation</u>
Volatiles	40%	60%
Dry Solids	40%	33%
Max. Combustible Solids, PPH	928	928
Max. Wet, PPH	5800	4687
Min. Combustible Solids, PPH	603	603
Min. Wet PPH	3770	3047

The above table shows the current operation as compared to the rates projected in 1979. The current operation maintains the volatile sludge solid rate which is the key design parameter. Because of the reduced ash recycle the dry solids feed rate and the wet solids feed rate change. See Appendix sheets G-4 and G-5 for graphic presentations of these changes.

Electric Power (Spec. 1Q 20.37K.)

Nine measurements by a joint test team (3 phases, 3 times on each motor) indicated an average total of 110.8 amps

Average Amps	L ₁	L ₂	L ₃	Ave
	111.2	110.8	110.5	110.8

$$\begin{aligned}\text{Power} &= (\text{Amps})(\text{Volts})(\text{P.F.})(\sqrt{3}) \\ &= (110.8)(488)(0.83)(1.737) \\ &= 77.7 \text{ Kw Actual} \qquad 200 \text{ Kw specified}\end{aligned}$$

Auxiliary Fuel (Spec 1Q 20.38)

During the pre-test meeting it was established that low-fire burners should be maintained for safety ignition and control purposes.

Fuel consumption during the test (0900 to 1600) averaged less than 0.1 GPM which equates to less than 0.8 mill BTU/hr. This is well within the normal allowance for ignition and control fuel.

The feed composition supplied during the test can be considered to be autogenous, with minimal fuel requirements for safety ignition and control purposes.

Warranty Test Procedure (Spec IQ 20.43)

The above specific paragraphs addressed the warranty requirements and show that the furnace is in compliance.

As part of the Emission Tests Envirotech normally takes other sample data for use in resolving any questions that may develop during evaluation of the data. These results are reported here as information.

Note: Moisture analyses used for the emission results were based on individual one-half hourly samples taken during the emission tests. The following are composite analyses:

Table 4-1. SUMMARY OF COMPOSITE SLUDGE, COMPOSITE ASH,
SCRUBBER WATER IN, AND SCRUBBER WATER OUT
ROCKY MOUNT WASTEWATER TREATMENT FACILITY

TRW #	Analysis	As received	Dry basis
<u>Composite sample 0900-1645</u>			
Sludge 4609	Ultimate analysis,		
	% Carbon		26.39
	% Hydrogen		0.27
	% Nitrogen		3.96
	% Sulfur	0.04	0.10
	% Ash	14.18	40.25
	Proximate analysis,		
	% Moisture	64.77	
	% Volatile Matter	20.08	
	% Fixed Carbon	0.97	
	Btu/lb	2182	6194
	Mercury (µg/gm)	0.328	
	Oxygen		29.03
<u>Composite sample 1100-1645</u>			
Sludge 4629	Ultimate analysis,		
	% Carbon		25.24
	% Hydrogen		0.23
	% Nitrogen		2.79
	% Sulfur	0.04	0.12
	% Ash	13.92	39.06
	Proximate analysis,		
	% Moisture	64.35	
	% Volatile Matter	21.08	
	% Fixed Carbon	0.65	
	Btu/lb	2269	6364
	Mercury (µg/gm)	0.187	
	Oxygen		32.56
Fuel oil 4617	% Ash	<0.01	
	% Sulfur	0.20	
	Btu/lb	18,736	
	Rams bottom carbon residue	0.185	

Air Pollution Test (spec IQ 20.47) & (Spec IQ 20.33)

The TRW report indicates that the system complies with EPA Code CFR 40, Part 60, Subpart O (which is the standard currently in effect and which was in effect at the time of bids).

SUMMARY OF PARTICULATE MATTER EMISSION TEST RESULTS:
INCINERATOR EXHAUST STACK - ROCKY MOUNT WASTEWATER TREATMENT PLANT

Test	Run #1 ^a	Run #2	Run #3	Run #4 ^b	Run #5
Date	1-13-83	1-13-83	1-13-83	1-13-83	1-13-83
Time	0940-1043	1105-1207	1235-1337	1410-1512	1537-1610
Sample Duration (min)	60	60	60	60	60
Sample Volume (DSCF)	N/A	53.562	55.268	64.151	60.601
Stack Flow (DSCFM)	N/A	3,916	4,120	4,782	4,488
Stack Temperature (°F)	N/A	98.8	98.6	99.1	99.9
Moisture (%)	N/A	5.9	3.1	5.0	4.7
CO ₂ (%)	N/A	4.92	5.25	6.68	4.51
O ₂ (%)	N/A	15.89	15.36	14.08	16.27
Excess Air (%)	N/A	317	274	206	350
Isokinetic (%)	N/A	98.9	97.0	N/A	97.6
Particulate Matter (lb/hr)	N/A	0.652	0.525	N/A	0.459
Feed Cake as % Dry Solids	32	33	32	32	32
Wet Feed Rate ^d (lb/hr)	5,000	5,000	5,300	5,300	5,300
Wet Feed Rate ^c (lb/hr)	N/A	3,946	4,419	N/A	3,997
Dry Feed Rate (ton/hr)	0.80	0.82	0.85	0.85	0.85
Dry Feed Rate ^e (ton/hr)	N/A	.651	.707	N/A	.64
Emission Rate (lbs/ton of dry feed)	N/A	0.79	0.62	N/A	0.54
Emission Rate ^e (lbs/ton of dry feed)	N/A	1.00	0.74	0.72	N/A
Visible Emissions (% opacity)	8.0	6.6	9.0	7.4	8.9

^aParticulate test invalid due to final leak check.

^bParticulate test was not valid. After the final leak check impinger water was sucked back into the filter.

^cVisible emissions were taken over the length of time particulate sample was being taken from the stack.

^dFeed rate was provided by Envirotech.

^eRate determination revised to account for process field measurement inaccuracy.

IV. TEST OPERATION, PROCEDURE, SAMPLING & ANALYSES

Furnace temperatures were maintained at typical levels. These are established by selectable set points on the temperature controllers. Temperatures are shown on the Log Sheet, which is included in Appendix B of the TRW Report.

Draft is controlled automatically by a control damper, and pressure drop through the venturi throat is selected by set point. Scrubber water rates and shaft speed were steady and within normal operating ranges, as shown on the log sheets.

Emission sampling and the analytical procedures for the material followed EPA methods as previously submitted and approved.

The feed rates used in this report are as preliminarily established in the field and as refined by analysis and calculation. Both procedures indicate acceptable emission levels. The refined rates were checked by a carbon balance which is as accurate as the code approved test procedures. These verified the corrected feed rate.

Sampling

Sludge samples were collected half-hourly and dry solids were determined by the TRW laboratory.

In addition, a composite sample was made for the test consisting of small samples taken at the same time as the individual samples. Hourly feed rate and fuel readings were taken. Routine samples were taken of the ash, scrubber water in and out and the fuel oil. The appearance of these was normal.

Complete stack samples were taken by TRW; details are included in the test lab report.

Analyses

All sample analyses were the responsibility of TRW.

V. APPENDAGE

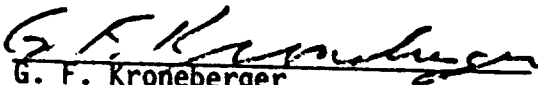
The official TRW report is appended to the official submittal copies of this report. That report contains the full details required by air pollution control agencies, and also contains field data detail.

The last appendix, Appendix G, of the TRW report was reserved for any appendix items that were supplied "by others", during the formulation of this report.

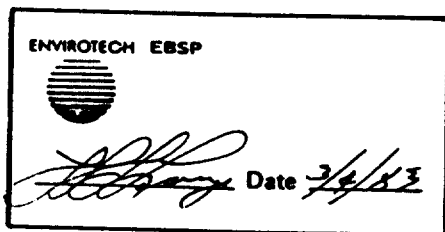
Appendix G contains the following:

- G-1 Feed rates calculated from TRW analyses and carbon balances
- G-2 Field calibration chart showing refined line correcting for conveyor lag
- G-3 Expanded scale chart suggested for future plant operation
- G-4 Chart showing revised feed composition
- G-5 Chart showing revised feed target corresponding to current feed composition.

PREPARED FEBRUARY 1983 BY:


G. F. Kroneberger
Principal Process Engineer
Lurgi Corporation

APPROVED BY



Hal Lange
Regional Manager



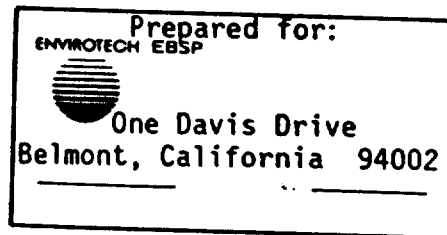
**ENERGY AND ENVIRONMENTAL DIVISION
TRW ENERGY DEVELOPMENT GROUP**

Redondo Beach, California • Research Triangle Park, North Carolina • McLean, Virginia • Denver, Colorado • Morgantown, West Virginia • Oakridge, Tennessee

SOURCE TESTING AND ANALYSIS
AT ROCKY MOUNT WASTEWATER TREATMENT FACILITY
ROCKY MOUNT, NORTH CAROLINA

P. #9002-5073-11
SN #95622.010
SN #540163

Technical Managers: Hal Lange
G. F. Kroneberger



February 1983

TRW Energy and Environmental Division
Post Office Box 13000
Research Triangle Park, North Carolina 27709

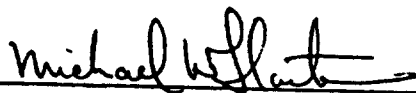
TABLE OF CONTENTS

	<u>Page</u>
1.0 INTRODUCTION.	1-1
2.0 SUMMARY AND DISCUSSION OF RESULTS	2-1
3.0 DISCUSSION OF RESULTS AND METHODS	3-1
4.0 COMPOSITE SLUDGES, ASH, SCRUBBER WATER AND FUEL OIL . . .	4-1
Appendix A - Calculations	A-1
Appendix B - Field Data	B-1
Appendix C - Field Analytical Data.	C-1
Appendix D - Laboratory Data	D-1
Appendix E - Equipment Calibration.	E-1
Appendix F - Personnel.	F-1

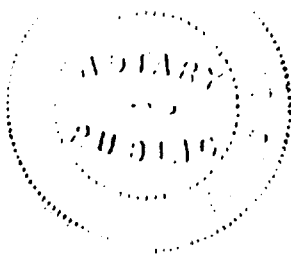
To Whom It May Concern:

I certify that I have read and reviewed the results, calculations and testing methods contained in the TRW report (February 1983) performed on January 13, 1983, "Source Testing and Analysis at Rocky Mount Wastewater Treatment Facility in Rocky Mount, North Carolina." The results and calculations are accurate based on the data obtained. The methods utilized are in conformance with EPA methods for testing sewage treatment plants. The only exception was the shortage of available sludge which required a shorter sampling duration of the sludge than normal.

Signed



Michael W. Hartman
Section Head, Field Services
TRW Energy and Environmental Division



My Commission Expires 5-20-87

1.0 INTRODUCTION

TRW Energy and Environmental Division, on January 13, 1983, conducted a source and analysis program at the Rocky Mount Wastewater Treatment Facility located near Rocky Mount, North Carolina under contract to the Envirotech Corporation (EBSP Division). The sewage sludge incinerator was tested for particulate matter emissions and odors, to determine compliance with the North Carolina State environmental regulations.

The emission tests consisted of a set of four test runs for determination of particulate matter emissions, stack opacity emissions, stack volumetric flowrate, and stack stationary gas analysis. Particulate matter, stack volumetric flowrate, opacity, and stack gas analysis were determined by standard EPA Methods 1, 2, 3, 5, and 9.

TRW conducted analysis on samples of feed, ash scrubber inlet, scrubber outlet, fuel and composite feed samples. The samples were collected by plant and test team personnel.

2. SUMMARY AND DISCUSSION OF RESULTS

Five one-hour long Method 5 tests were run on the incinerator exhaust stack. At the end of the first test it was discovered that the last impinger had opened during the test. This test was voided. At the end of the fourth test, impinger water was inadvertently flushed back into the filter. This test was also voided but analyzed for future knowledge. No known problems were encountered during tests #2, #3 and #5. The average emission rate for these three tests was 0.65 pounds for each ton of dry sludge fired as compared to the allowable standard of 1.30 pounds per ton dry sludge. A summary of the results can be found in Table 2-1. The wet feed rates and sludge samples were provided by Envirotech.

Opacity readings were taken during the time that each test was being run. The average for all five tests is 8.0% opacity with no readings being higher than 20.0%.

No odors that could be traced to the exhaust stack at a fifty foot distance were noticed while the testers were on the roof. A very slight smell was noticed in gas bag samples, when they were directly blown at the tester's nose.

The sludge samples as fired were taken each half hour and analyzed for moisture by standard method 209A. The results are reported in Table 2-2.

**Table 2-1. SUMMARY OF PARTICULATE MATTER EMISSION TEST RESULTS:
INCINERATOR EXHAUST STACK - ROCKY MOUNT WASTEWATER TREATMENT PLANT**

Test	Run #1 ^a	Run #2	Run #3	Run #4 ^b	Run #5
Date	1-13-83	1-13-83	1-13-83	1-13-83	1-13-83
Time	0940-1043	1105-1207	1235-1337	1410-1512	1537-1610
Sample Duration (min)	60	60	60	60	60
Sample Volume (DSCF)	N/A	53.562	55.268	64.151	60.601
Stack Flow (DSCFM)	N/A	3,916	4,120	4,782	4,488
Stack Temperature (°F)	N/A	98.8	98.6	99.1	99.9
Moisture (%)	N/A	5.9	3.1	5.0	4.7
CO ₂ (%)	N/A	4.92	5.25	6.68	4.51
O ₂ (%)	N/A	15.89	15.36	14.08	16.27
Excess Air (%)	N/A	317	274	206	350
Isokinetic (%)	N/A	98.9	97.0	N/A	97.6
Particulate Matter (lb/hr)	N/A	0.652	0.525	N/A	0.459
Feed Cake as % Dry Solids	32	33	32	32	32
Wet Feed Rate ^d (lb/hr)	5,000	5,000	5,300	5,300	5,300
Wet Feed Rate ^c (lb/hr)	N/A	3,946	4,419	N/A	3,997
Dry Feed Rate (ton/hr)	0.80	0.82	0.85	0.85	0.85
Dry Feed Rate ^e (ton/hr)	N/A	.651	.707	N/A	.64
Emission Rate (lbs/ton of dry feed)	N/A	0.79	0.62	N/A	0.54
Emission Rate ^e lbs/ton or dry feed)	N/A	1.00	0.74	0.72	N/A
Visible Emissions (% opacity) ^c	8.0	6.6	9.0	7.4	8.9

^a Particulate test invalid due to final leak check.

^b Particulate test was not valid. After the final leak check impinger water was sucked back into the filter.

^c Visible emissions were taken over the length of time particulate sample was being taken from the stack.

^d Feed rate was provided by Envirotech.

^e Rate determination revised to account for process field measurement inaccuracy.

Table 2-2. ANALYTICAL RESULTS - FURNACE FEED % MOISTURE

Sample Time	% Moisture*
0800	66
0830	68
0900	68
0930	69
1000	67
1030	70
1100	67
1130	66
1200	67
1230	67
1300	68
1330	70
1400	68
1430	66
1500	68
1530	69
1600	67
1630	67
1645	69

*Standard Method 209A.

3. DISCUSSION OF METHODS

3.1 PARTICULATE MATTER EMISSION TESTS

Particulate matter emissions were determined according to standard Environmental Protection Agency (EPA) Methods 1, 2, 3, and 5.

EPA Method 1

The criteria described in EPA Reference Method 1 (Sample and Velocity Traverses for Stationary Sources Federal Register 42 FR 41754, August 18, 1977) were used to select appropriate sampling sites. The eight diameters and two diameters rule, upstream and downstream, respectively, of any flow disturbance is the primary criteria. The sampling points were located more than 8 duct diameters upstream from the nearest flow disturbance and 2 duct diameters downstream from the stack exit. Twelve points were sampled at 5 minutes a point for 1 hour of total test time. A diagram of the incinerator exhaust stack location is shown in Figure 3-1. The traverse points for the stack were calculated and reported on a standardized form (Appendix B - Field Data Sheets).

EPA Method 2

EPA Reference Method 2 (Determination of Stack Gas Velocity and Volumetric Flow Rate, Federal Register 42 FR 41759, August 18, 1977) was followed to determine flue gas velocity, stack temperature, stack pressure, and volumetric flow rate. A check for cyclonic flow was made. The flow was not cyclonic.

EPA Method 3

EPA Reference Method 3 (Gas Analysis, for Carbon Dioxide, Oxygen, Excess Air, and Dry Molecular Weight - Federal Register 42 FR 41768) was utilized to characterize the stationary gas analysis. As permitted under Section 1.2, paragraph 2 of the reference document a modification to the sampling procedures and use of an alternative analytical procedure was implemented. A single point integrated sample was collected. In

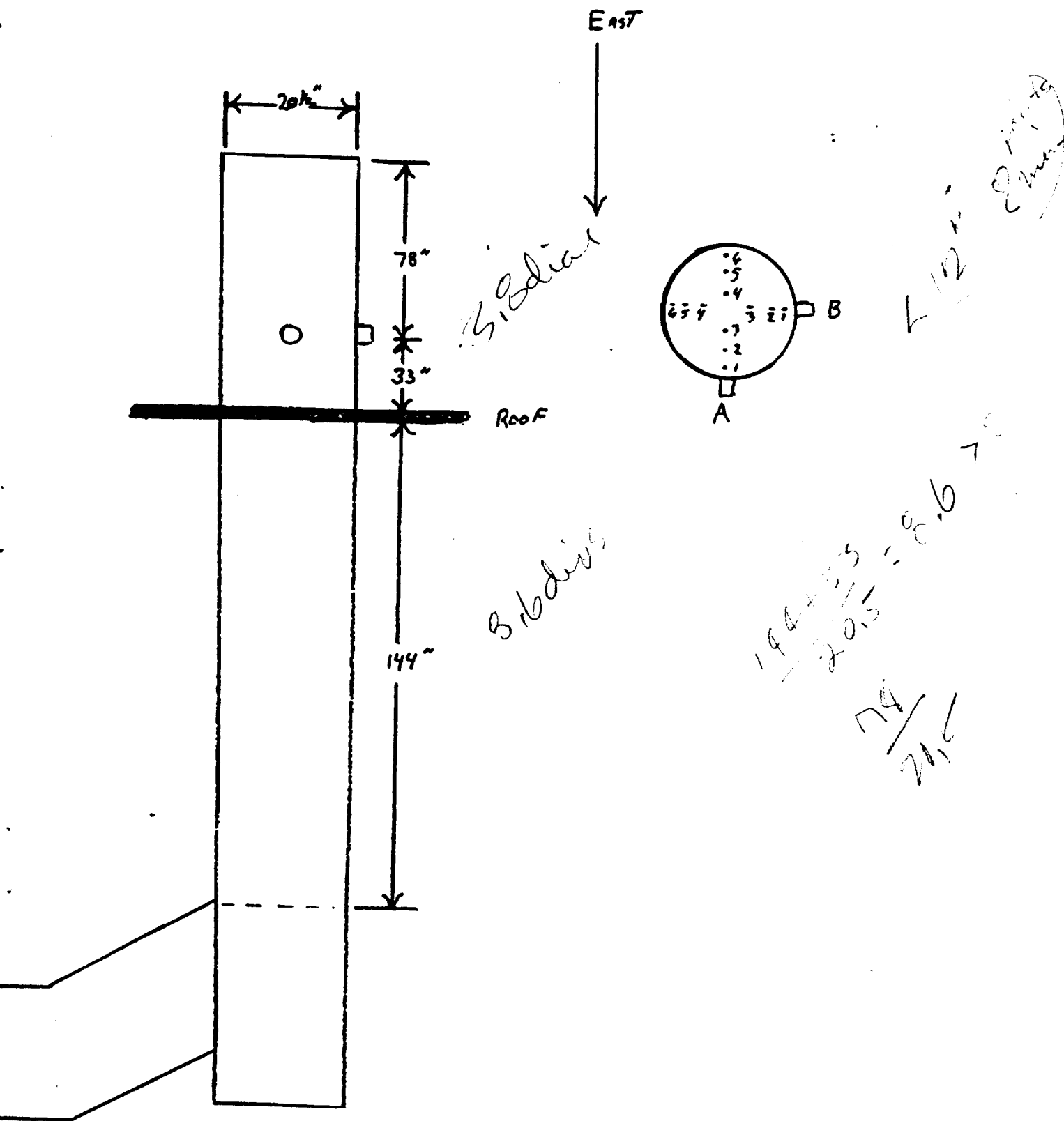


Figure 3-1. Diagram of sampling locations - incinerator exhaust stack.

lieu of an Orsat analyzer, a gas chromatograph with a thermal conductivity detector (GC/TCD) was utilized to measure the concentrations of oxygen (O_2), carbon dioxide (CO_2), and nitrogen (N_2) in the integrated bag sample.

Helium was the carrier gas. Compound separation was achieved with a packed stainless steel Chromosorb 102/Molecular Sieve column. Calibration gas standards was injected prior to and after sample by injection for a quantification by retention time and peak area. A one point calibration method was employed utilizing a Scotty II-Mix 35 calibration mixture ($\pm 2\%$ certified). This mixture contains stationary gas components as follows:

- CO_2 - 2.88%
- O_2 - 16.8%
- N_2 - 80.3%

EPA Method 5

EPA Reference Method 5 - (Determination of Particulate Emissions from Stationary Sources - Federal Register 42 FR 41776, August 18, 1977) was utilized to measure particulate matter in the flue gas streams. The particulate mass, which includes any material that condenses at or above the filtration temperature, is determined gravimetrically after removal of uncombined water. The filter box temperature of $250^\circ F \pm 25^\circ F$ was used. The operating and maintenance procedures for the sampling train was followed as described in APTD-0576. Quality control procedures have been implemented to ensure proper calibration and operation techniques. Equipment calibration forms are in Appendix E. Figure 3-2 is a schematic illustration of the EPA Method 5 sampling train.

EPA Method 9

EPA Reference Method 9 - (Visual Determination of the Opacity of Emissions from Stationary Sources - Federal Register 42 FR 41776, August 18, 1977) was utilized to measure the percent opacity of the stack gas. This was based on 15 second readings during the 1 hour Method 5 test.

3.2 SLUDGE

Samples were taken by grab sampling according to standard sampling methods.

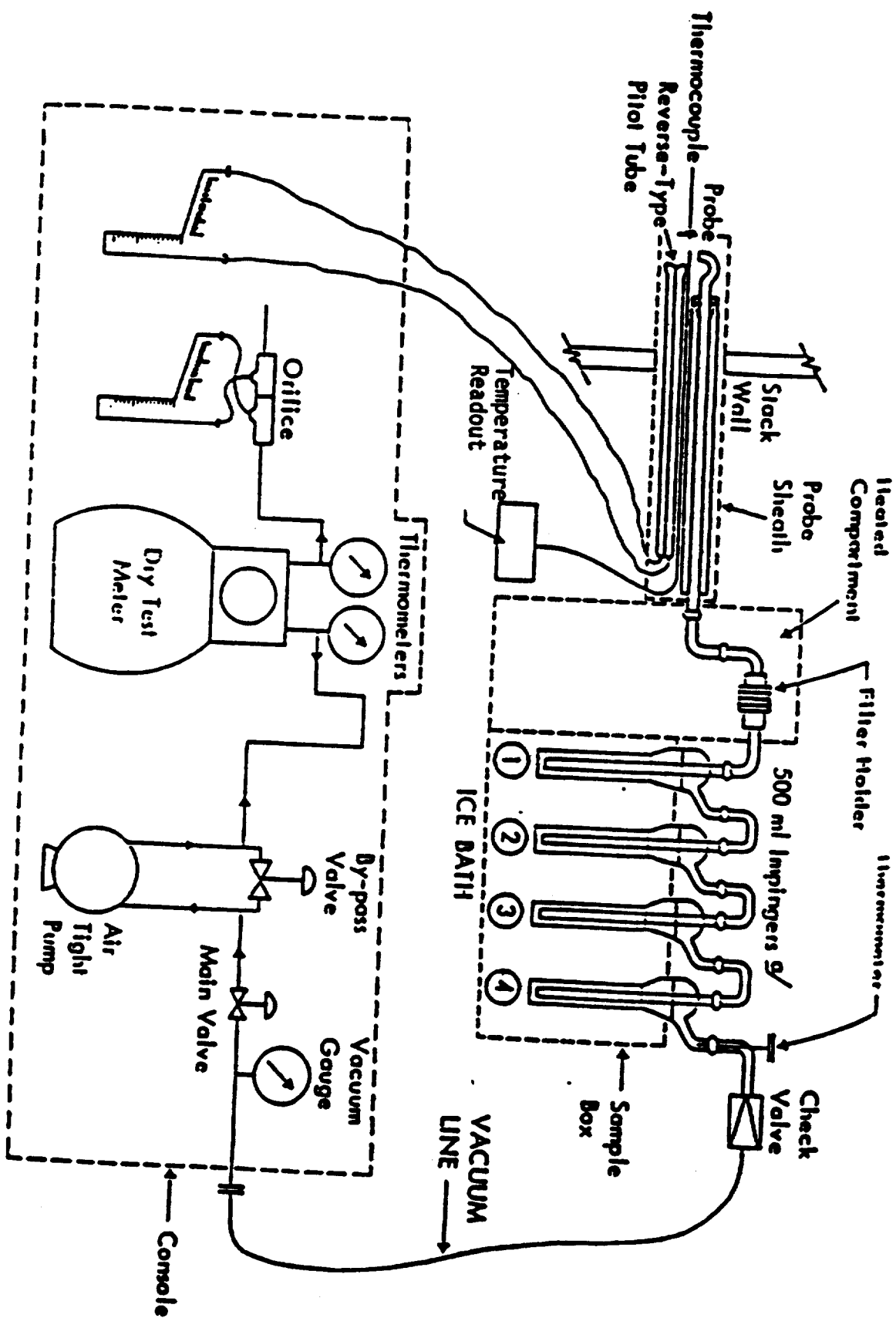


Figure 3-2. Schematic illustration of EPA Method 5 sampling train.

4.0 COMPOSITE SLUDGES, ASH, SCRUBBER WATER AND FUEL OIL

The samples were taken by Lurgi personnel, composited by TRW personnel, and analyzed by an independent laboratory. The results are reported in Table 4-1.

SAMPLE ANALYSIS SCHEDULE

Test lab samples are to be analyzed as follows:

Sludge Samples: (3 each)

One composite sample for each test day is to be analyzed as follows:

1. Proximate: ASTM D3172-73 (Low temperature determination of volatiles)
2. Ultimate: ASTM D3176-74
3. Heating Value: ASTM D2015-66
4. Mercury

Ash Sample: (1 each)

A composite ash sample is to be analyzed per ASTM D3172-73.

Scrubber Water: (2 each)

Inlet and outlet scrubber water samples are to be analyzed as follows:

1. Settleable Solids: Standard Methods 208F
2. Total Suspended Solids: Standard Methods 208D
3. Total Solids (including dissolved): Standard Methods 208A

Fuel Oil: (1 each)

General reference specification for fuel oil is ASTM D-396-73.
Specific tests to be performed are:

Moisture and Sediment	D-473-69
Residual Carbon	D-524
Sulfur	D-129
Heat Value	D-240-72
Ash	D-482-73

March 9, 1983

SUPPLEMENTAL
Table 4-1. SUMMARY OF COMPOSITE SLUDGE, COMPOSITE ASH,
SCRUBBER WATER IN, AND SCRUBBER WATER OUT
INCINERATOR EXHAUST STACK - ROCKY MOUNT WASTEWATER TREATMENT FACILITY

TRW #	Analysis	As received	Dry basis
TRW # 4609 Sludge 0800-1645 1-13-83	Ultimate analysis, Weight % Carbon Weight % Hydrogen Weight % Nitrogen Weight % Oxygen Weight % Sulfur Weight % Ash	 0.04 14.18	 26.39 0.27 3.96 29.03 0.10 40.25
	Proximate analysis, Weight % Moisture Weight % Ash Weight % Volatile Matter	 64.77 14.18 20.08	 40.25
	Weight % Fixed Carbon Btu/lb	 0.97 2182	 6194
TRW # 4629 Sludge 1100-1645 1-13-83	Ultimate analysis, Weight % Carbon Weight % Hydrogen Weight % Nitrogen Weight % Oxygen Weight % Sulfur Weight % Ash	 0.04 13.92	 25.24 0.23 2.79 32.56 0.12 39.06
	Proximate analysis, Weight % Moisture Weight % Ash Weight % Volatile Matter Weight % Fixed Carbon Btu/lb	 64.35 13.92 21.08 0.65 2269	 39.06 6364
TRW # 4628 Ash	Proximate Analysis Weight % Moisture Weight % Ash Weight % Volatile Matter Sulfur	 28.56 60.24 0 <.01	 84.32 0

(continued)

Table 4-1. Concluded

TRW #	Analysis	As received	Dry basis
TRW # 4615 Scrubber in	Total Solids (mg/l)	625	
	Total Suspended Solids (mg/l)	41	
	Settleable Solids (mg/l/hr)	<0.1	
TRW # 4616 Scrubber out	Total Solids (mg/l)	1040	
	Total Suspended Solids (mg/l)	101	
	Settleable Solids (mg/l/hr)	<0.1	
TRW # 4617 Fuel oil	Weight % Ash ^a	<0.01	
	Weight % Sulfur ^b	0.20	
	Btu/lb ^c	18,736	
	Weight % Rams bottom carbon residue ^d	0.185	
TRW # 4629 Sludge	Mercury (µg/g) ^e	0.187	
TRW # 4609 Sludge	Mercury (µg/g) ^e	0.328	

^a Determined by method ASTM D-482-73.

^b Determined by method ASTM D-129.

^c Determined by method ASTM D-240-72.

^d Determined by method ASTM D-524.

* Volatile matter and ash were determined at 550°C.

^e Determined by Method EPA 105 by Grainger Labs.

APPENDIX A
SAMPLE PARTICULATE CALCULATION

SAMPLE PARTICULATE CALCULATIONS

1. Volume of dry gas sampled at standard conditions - 70°F, 29.92" Hg, ft³.

$$V_{m_{std}} = \frac{17.64 \times V_m \cdot \frac{P_B + P_m}{13.6}}{(T_m + 460)} = \text{ft}^3 =$$

2. Volume of water vapor at 70°F and 29.92" Hg, ft³.

$$V_{w_{gas}} = 0.0471 \times V_w = \text{ft}^3$$

3. % moisture in stack gas

$$\%M = \frac{100 \times V_{w_{gas}}}{V_{m_{std}} + V_{w_{gas}}} = \%$$

4. Mole fraction of dry gas

$$M_d = \frac{100 - \%M}{100}$$

5. Average molecular weight of dry stack gas

$$M W_d = (\%CO_2 \times \frac{44}{100}) + (\%O_2 \times \frac{32}{100}) + (\%N_2 \times \frac{28}{100})$$

^aThe variations between these calculations and those used as shown on the load sheets are due to rounding in these manual calculations.

6. Molecular weight of stack gas

$$MW = MW_d \times M_d + 18 (1 - M_d)$$

7. Stack velocity @ stack conditions, fpm

$$V_s = 4310 \times \frac{\Delta P_s \times (T_s + 460)}{P_s \times MW}^{1/2} = \text{fpm}$$

8. Stack gas volume @ actual conditions

$$ACFM = \frac{V_s \times A_s}{144}$$

9. Stack gas volume @ standard conditions (DSCFM)

$$Q_s = \frac{0.123 \times V_s \times A_s \times M_d \times P_s}{(T_s + 460)} = \text{DSCFM}$$

10. Percent isokinetic

$$\%I = \frac{1032 \times (T_s + 460) \times V_{mstd}}{V_s \times T_t \times P_s \times M_d \times (D_n)^2} = \%$$

11. Particulate - probe, cyclone, and filter (gr/DSCF)

$$C_{an} = 0.0154 \times \frac{M_f}{V_{mstd}} = \text{gr/DSCF}$$

12. Particulate - probe, cyclone and filter, gr/ACF at stack conditions

$$C_{at} = \frac{17.7 \times C_{an} \times P_s \times M_d}{(T_s + 460)} = \text{gr/ACF}$$

13. Particulate - probe, cyclone, filter, lb/hr.

$$C_{aw} = 0.00857 \times C_{ah} \times Q_s = \text{lb/hr.}$$

14. Particulate - probe, cyclone, and filter, gr/DSCF corrected to 12 percent CO₂

$$\frac{12}{\text{Stack CO}_2} \times C_{an} = \text{gr/DSCF corrected to 12\% CO}_2$$

15. Particulate - probe, cyclone and filter, gr/ACF at stack conditions

$$C_{at} = \frac{17.7 \times C_{an} \times P_s \times M_d}{(T_s + 460)} = \text{gr/ACF}$$

16. Particulate - probe, cyclone, filter, lb/hr.

$$C_{aw} = 0.00857 \times C_{ah} \times Q_s = \text{lb/hr.}$$

Particulate Nomenclature.

A_n	= Cross-sectional area of nozzle, m^2 (ft^2).
A_s	= Cross-sectional area of stack, m^2 (ft^2).
B_{ws}	= Water vapor in the gas stream, proportion by volume.
C_a	= Acetone blank residue concentration, mg/g.
C_{act}	= Concentration of particulate matter in stack gas, at stack conditions (gr/ACF).
C_{std}	= Concentration of particulate matter in stack gas, dry basis, corrected to standard conditions, g/dscm (g/dscf).
E	= Particulate matter emission rate (lb/hr).
I	= Percent of isokinetic sampling.
L_a	= Maximum acceptable leakage rate for either a pretest leak check or for a leak check following a component change; equal to $0.00057 m^3/min$ ($0.02 cfm$) or 4 percent of the average sampling rate, whichever is less.
L_i	= Individual leakage rate observed during the leak check conducted prior to the " i^{th} " component change ($i = 1, 2, 3, \dots, n$), m^3/min (cfm).
L_p	= Leakage rate observed during the post-test leak check, m^3/min (cfm).
K_p	= Pitot tube constant.
M_d	= Mole fraction of dry gas.
M_f	= Particulate matter collected in sampling train (probe, cyclone and filter) in milligrams (mg).
m_n	= Total amount of particulate matter collected, mg.
MW_a	= Average molecular weight of dry stack gas.
M_w	= Molecular weight of water, $18.0 g/g\text{-mole}$ ($18.0 lb/lb\text{-mole}$).
MW	= Molecular weight of stack gas (wet).
m_a	= Mass of residue of acetone after evaporation, mg.
P_{bar}	= Barometric pressure at the sampling site, mm Hg (in. Hg).
P_s	= Stack static pressure, mmHg (in. Hg).
P_s	= Absolute stack gas pressure, mm Hg (in. Hg).
	= $P_{bar} + P_g$
P_{std}	= Standard absolute pressure, 760 mm Hg (29.92 in. Hg).

- Q_{sd} = Dry volumetric stack gas flow rate corrected to standard conditions, dscm (dscf).
- R = Ideal gas constant, 0.06236 mm Hg-m³/°K-g-mole (21.85 in. Hg-ft³/°R-lb-mole).
- T_m = Absolute average dry gas meter temperature, °K (°R).
- T_s = Absolute average stack gas temperature (see Figure 5-2), °K (°R).
- T_{std} = Standard absolute temperature, 293°K (528°R).
- T_t = Total time of process feed rate determination (min).
- V_a = Volume of acetone blank, ml.
- V_{aw} = Volume of acetone used in wash, ml.
- V_{lc} = Total volume of liquid collected in impingers and silica gel, ml.
- V_m = Volume of gas sample as measured by dry gas meter, dcm (dcf).
- $V_{m(std)}$ = Volume of gas sample measured by the dry gas meter, corrected to standard conditions, dscm (dscf).
- $V_{w(std)}$ = Volume of water vapor in the gas sample, corrected to standard conditions, scm (scf).
- V_s = Stack gas velocity, calculated by Method 2, using data obtained from Method 5, m/sec (ft/sec).
- W_a = Weight of residue in acetone wash, mg.
- Y = Dry gas meter calibration factor.
- ΔH = Average pressure differential across the orifice meter (see Figure 5-2), mm H₂O (in. H₂O).
- ΔP = Velocity head of stack gas, mmH₂O (in H₂O).
- ρ_a = Density of acetone, mg/ml.
- ρ_w = Density of water, 0.9982 g/ml (0.002201 lb/ml).
- θ = Total sampling time, min.
- θ_1 = Sampling time interval, from the beginning of a run until the first component change, min.
- θ_i = Sampling time interval, between two successive component changes, beginning with the interval between the first and second changes, min.

- θ_p = Sampling time interval, from the final (n^{th}) component change until the end of the sampling run, min.
 13.6 = Specific gravity of mercury.
 60 = Sec/min.
 4310 = Conversion factor: Pitot tube coefficient (C_p) X Pitot tube constant (K_p) X 60, where $K_p = 85.49$ and $C_p = .84$.
 2000 = Conversion pound to ton.
 100 = Conversion to percent.

LOAD SHEET
STACK TEST - PARTICULATE

Test # 2

Part 1

Enter	(Initial y Only)	
	Value	Location
	0.028317	04
	17.64	05
	.0471	06
	1032	07

Test # 3

Test # 4

Enter	Value	Location	Enter	Value	Location	Enter	Value	Location
T _r (Min)	60	09	T _r (Min)	60	09	T _r (Min)	60	09
(DN) ² (in ²)	.0961	10	(DN) ² (in ²)	.0961	10	(DN) ² (in ²)	.0961	10
PS(in Hg)	30.18	11	PS(in Hg)	30.18	11	PS(in Hg)	30.18	11
VM(ft ³)	53.323	12	VM(ft ³)	55.000	12	VM(ft ³)	63.77	12
VW(ml)	71.5	13	VW(ml)	38.	13	VW(ml)	71.6	13
% CO ₂	4.92	14	% CO ₂	5.25	14	% CO ₂	6.68	14
% O ₂	15.89	15	% O ₂	15.36	15	% O ₂	14.08	15
% N ₂	79.19	16	% N ₂	79.39	16	% N ₂	79.24	16
4310V	56200.67	17	4310V	57751.04	17	4310V	68345.69	17
As(ft ²)	2.29	18	As(ft ²)	2.29	18	As(ft ²)	2.29	18
(Ts+460)	558.8	19	(Ts+460)	558.6	19	(Ts+460)	559.1	19
Part 2			Part 2			Part 2		
mf (mg)		00	mf (mg)		00	mf (mg)		00
mt (mg)	67.6	01	mt (mg)	53.4	01	mt (mg)	79.3	01
VMSTD(ft ³)	53.562	02	VMSTD(ft ³)	55.268	02	VMSTD(ft ³)	64.151	02
Ps ("Hg)	30.18	03	Ps ("Hg)	30.18	03	Ps ("Hg)	30.18	03
Md	0.941	04	Md	.969	04	Md	0.950	04
(Ts+460)	558.8	05	(Ts+460)	558.6	05	(Ts+460)	559.1	05
Qs(scfm)	3916.5	06	Qs(scfm)	4120.0	06	Qs(scfm)	4781.7	06
Tm	74.2		Tm	74.2		Tm	75.2	
Pm	2.95		Pm	3.14		Pm	4.37	
Pb	30.20		Pb	30.20		Pb	30.20	

RESULTS
STACK TEST - PARTICULATE

Test # 2		Test # 3		Test # 4	
Value		Value		Value	
Vm (DSCF)	53.542	Vm (DSCF)	55.268	Vm (DSCF)	64.151
Vm (DSCM)	1.516	Vm (DSCM)	1.564	Vm (DSCM)	1.815
Vw gas (SCF)	3.368	Vw gas (SCF)	1.790	Vw gas (SCF)	3.372
% Moisture	5.915	% Moisture	3.137	% Moisture	4.994
Md	0.941	Md	0.969	Md	0.950
MWd	29.423	MWd	29.454	MWd	29.632
MW	28.742	MW	29.095	MW	29.051
Vs (fpm)	1908.029	Vs (fpm)	1948.903	Vs (fpm)	2308.164
ACFM	4369.4	ACFM	4463.0	ACFM	5285.7
Flow (DSCFM)	3916.5	Flow (DSCFM)	4120.0	Flow (DSCFM)	4751.7
Flow (DSCMM)	110.84	Flow (DSCMM)	116.60	Flow (DSCMM)	135.32
% I	98.9	% I	97.0	% I	97.0
% EA	316.8	% EA	274.3	% EA	205.9
Front gr/dscf	—	Front gr/dscf	—	Front gr/dscf	—
Front gm/dscm	—	Front gm/dscm	—	Front gm/dscm	—
Total gr/dscf	0.01944	Total gr/dscf	0.01458	Total gr/dscf	0.01904
Total gm/dscm	0.04451	Total gm/dscm	0.03407	Total gm/dscm	0.04359
Front gr/acf	—	Front gr/acf	—	Front gr/acf	—
Front gm/acm	—	Front gm/acm	—	Front gm/acm	—
Total gr/acf	0.01742	Total gr/acf	0.01374	Total gr/acf	0.01722
Total gm/acm	0.03990	Total gm/acm	0.03147	Total gm/acm	0.03943
Front lb/hr	—	Front lb/hr	—	Front lb/hr	—
Front kg/hr	—	Front kg/hr	—	Front kg/hr	—
Total lb/hr	0.652	Total lb/hr	0.525	Total lb/hr	0.790
Total kg/hr	0.296	Total kg/hr	0.238	Total kg/hr	0.354

LOAD SHEET
STACK TEST - PARTICULATE

Test # 5

Part 1						Part 2		
Enter	(Initial Value)	Location	Enter	Value	Location	Enter	Value	Location
	0.028317	04						
	17.64	05						
	.0471	06						
	1032	07						
$T_f(\text{Min})$	60	09	$T_f(\text{Min})$		09	$T_f(\text{Min})$		09
$(DN)^2(\text{in}^2)$	.0961	10	$(DN)^2(\text{in}^2)$		10	$(DN)^2(\text{in}^2)$		10
PS(in Hg)	30.18	11	PS(in Hg)		11	PS(in Hg)		11
VH(ft ³)	60.490	12	VH(ft ³)		12	VH(ft ³)		12
VW(ml)	64.0	13	VW(ml)		13	VW(ml)		13
% CO ₂	4.51	14	% CO ₂		14	% CO ₂		14
% O ₂	16.27	15	% O ₂		15	% O ₂		15
% N ₂	79.22	16	% N ₂		16	% N ₂		16
4310V	63824.19	17	4310V		17	4310V		17
As(ft ²)	2.29	18	As(ft ²)		18	As(ft ²)		18
(Ts+460)	559.9	19	(Ts+460)		19	(Ts+460)		19
	Part 2			Part 2			Part 2	
mf (mg)		00	mf (mg)		00	mf (mg)		00
mt (mg)	47.0	01	mt (mg)		01	mt (mg)		01
VMSTD(ft ³)	60.601	02	VMSTD(ft ³)		02	VMSTD(ft ³)		02
Ps ("Hg)	30.18	03	Ps ("Hg)		03	Ps ("Hg)		03
Md	0.953	04	Md		04	Md		04
(Ts+460)	559.9	05	(Ts+460)		05	(Ts+460)		05
Os(scfm)	4487.8	06	Os(scfm)		06	Os(scfm)		06
Tm	76.7		Tm			Tm		
Pm	3.82		Pm			Pm		
Pb	30.20		Pb			Pb		

RESULTS
STACK TEST - PARTICULATE

Test # 5		Test #		Test #	
Value		Value		Value	
Vm (DSCF)	60.601	Vm (DSCF)		Vm (DSCF)	
Vm (DSCM)	1.715	Vm (DSCM)		Vm (DSCM)	
Vw gas (SCF)	3.014	Vw gas (SCF)		Vw gas (SCF)	
% Moisture	4.738	% Moisture		% Moisture	
Md	0.953	Md		Md	
MWd	29.372	MWd		MWd	
MW	28.834	MW		MW	
Vs (fpm)	2163.599	Vs (fpm)		Vs (fpm)	
ACFM	4954.6	ACFM		ACFM	
Flow (DSCFM)	4487.8	Flow (DSCFM)		Flow (DSCFM)	
Flow (DSCMM)	127.01	Flow (DSCMM)		Flow (DSCMM)	
% I	97.6	% I		% I	
% EA	350.3	% EA		% EA	
Front gr/dscf	—	Front gr/dscf		Front gr/dscf	
Front gm/dscm	—	Front gm/dscm		Front gm/dscm	
Total gr/dscf	0.01194	Total gr/dscf		Total gr/dscf	
Total gm/dscm	0.02735	Total gm/dscm		Total gm/dscm	
Front gr/acf	—	Front gr/acf		Front gr/acf	
Front gm/acm	—	Front gm/acm		Front gm/acm	
Total gr/acf	0.01082	Total gr/acf		Total gr/acf	
Total gm/acm	0.02478	Total gm/acm		Total gm/acm	
Front lb/hr	—	Front lb/hr		Front lb/hr	
Front kg/hr	—	Front kg/hr		Front kg/hr	
Total lb/hr	0.459	Total lb/hr		Total lb/hr	
Total kg/hr	0.208	Total kg/hr		Total kg/hr	

APPENDIX B

FIELD DATA

TRW
ENVIRONMENTAL ENGINEERING DIVISION

NOMOGRAPH DATA

PLANT Rocky Mount
DATE 1-13-83
SAMPLING LOCATION Incinerator Exhaust

CALIBRATED PRESSURE DIFFERENTIAL ACROSS ORIFICE, in. H ₂ O	ΔH_0	1.95
AVERAGE METER TEMPERATURE (AMBIENT + 20°F), °F	$T_{m, avg.}$	70
PERCENT MOISTURE IN GAS STREAM BY VOLUME	B_{wv}	5
BAROMETRIC PRESSURE AT METER, in. Hg	P_m	30.20
STATIC PRESSURE IN STACK, in. Hg H ₂ O ($P_m \pm 0.073 \times$ STACK GAUGE PRESSURE in in. H ₂ O)	P_s	-0.22
RATIO OF STATIC PRESSURE TO METER PRESSURE	P_s/P_m	1.0
AVERAGE STACK TEMPERATURE, °F	$T_{s, avg.}$	100
AVERAGE VELOCITY HEAD, in. H ₂ O	$\Delta P_{avg.}$	0.25
MAXIMUM VELOCITY HEAD, in. H ₂ O	$\Delta P_{max.}$	0.32
C FACTOR		1.08
CALCULATED NOZZLE DIAMETER, in.		5/16
ACTUAL NOZZLE DIAMETER, in.		0.310
REFERENCE Δp , in. H ₂ O		0.19

EPA (Dwt) 234
4 72

TRAVERSE POINT LOCATION FOR CIRCULAR DUCTS

SCHEMATIC OF SAMPLING LOCATION

B-2

PRELIMINARY VELOCITY TRAVERSE

PLANT Rocky Mount
DATE 1-13-83
LOCATION Incinerator Exhaust
STACK I.D. 20.5"
BAROMETRIC PRESSURE, in. Hg 30.20
STACK GAUGE PRESSURE, in. H₂O ~~1.00~~ .22
OPERATORS MCR DS

Not Cyclonic Flow

[illegible]

EPA (Dwr) 233
4/72

SCHEMATIC OF TRAVERSE POINT LAYOUT

[illegible]

FIELD DATA

IN Valid

HEATER ROOM SETTING 3:50
 FIRE/ LEAK NO. 866
 SCHEMATIC OF TRAVERSE POINT LAYOUT
 NO RECORD ALL DATA EVERY MINUTES
 LEAK AT S.G. TAP.

READ AND RECORD ALL CATS EVERY

TRAVEL POINT NUMBER	SAMPLING TIME, min	CLOCK TIME (AM or PM)	GAS METER READING (ft ³ , ft ³)	VELOCITY HEAD (in. H ₂ O)	ORIFICE PRESSURE (in. H ₂ O)		STACK TEMPERATURE (°F)	ORIFICE METER TEMPERATURE (°F)		PUMP VACUUM, in. Hg	SAMPLE BOX TEMPERATURE, °F	IMPROVER TEMPERATURE, °F
					DESIRED	ACTUAL		INLET (ft ³ , ft ³)	OUTLET (ft ³ , ft ³)			
	0	0940	403.802									
A-1	5	45	402.40	.40	2.0	2.0	99	52	52	1	238	40
2	10	50	411.15	.33	2.1	2.1	100	62	54	1	242	36
3	15	55	414.8	.31	2.0	2.0	101	70	50	1	236	38
4	20	1000	419.7	.28	2.5	2.4	95	74	58	1	236	35
5	25	05	422.8	.35	3.4	3.4	96	78	60	1	250	36
6	30	10	428.685	.36	3.5	3.5	96	79	62	1	232	36
3405	30	1013	428.685	.34	2.2	2.2	94	77	60	1	245	34
B-1	35	18	432.85	.24	2.2	2.2	95	74	62	1	246	38
2	40	23	436.80	.23	2.2	2.2	96	74	62	1	245	34
3	45	28	440.82	.27	2.6	2.6	97	76	62	1	243	36
4	50	33	445.02	.26	2.5	2.5	96	78	64	1	243	35
5	55	38	449.60	.32	3.1	3.1	98	90	64	1	243	36
6	60	1043	454.758	.39	3.8	3.8	97	84	60	1	245	35

COMME 175.

CPA-001775

FIELD DATA

PROBE LENGTH AND TYPE 41 53
NOZZLE I.D. 2.319
ASSUMED DENSITY 1.5
SAMPLE DRY NUMBER 76
TESTER DRY NUMBER 95
WATER AN 1.95
E-FACTOR 1.69
PROBE HEATING SETTING 70.8
HEATING DRY SETTING 2.510
TESTING RATE 49 219

SCHEMATIC OF TRAVERSE POINT LAYOUT

SCHEMATIC OF TRAVERSE POINT LAYOUT

READ AND RECORD ALL DATA EVERY _____ MINUTES

Pre-book Check 0015 at 13°

Final 0015 0150

TRAVERSE POINT NUMBER	SAMPLING TIME, min	CLOCK TIME (in m. clock)	GAS METER READING ($W_{g, 1}$)	VELOCITY HEAD ($W_{g, 2}$) in. H ₂ O	DIFFERENCE ($W_{g, 1} - W_{g, 2}$)		STACK TEMPERATURE (T_s) °F	OXYGEN METER		PUMP VACUUM in. Hg	SAMPLE BOX TEMPERATURE, °F	IMPELLER TEMPERATURE, °F
					DESIRED	ACTUAL		INLET (O_2) %	OUTLET (O_2) %			
B-1	0	11:05	456.352									
2	5	10	460.005	1.23	2.2	2.2	99	63	62	7	210	40
3	10	15	464.15	1.25	2.4	2.4	98	72	62	7	218	40
4	15	20	468.26	1.27	2.6	2.6	102	78	64	8	223	44
5	20	25	472.60	1.28	2.7	2.7	98	82	68	9	225	46
5	25	30	477.15	1.33	3.2	3.2	99	85	66	10	222	48
5	30	35	482.119	1.35	3.7	3.7	99	88	66	12	228	48
START	30	11:30	482.119									
1	35	41	486.80	1.24	2.1	2.1	97	84	66	8	213	52
2	40	47	490.15	1.25	2.4	2.4	99	84	68	8	230	52
3	45	52	494.45	1.25	2.7	2.7	101	86	65	9	238	52
4	50	58	499.40	1.37	3.6	3.6	95	88	65	12	231	56
5	55	1:02	504.46	1.40	3.2	3.2	98	90	65	14	234	56
6	60	07	509.675	1.41	4.0	4.0	98	90	70	14	235	56
	60		53.323 ✓			2.98	98.8	74.25 ✓				
			562.07.67	6.2 ✓				6.25 (6.6)				
				1.2 ✓								
				1.5472								

71.5 mL.

5342

FIELD DATA

PLANT: Rocky Mount
DATE: 1-13-52
SAMPLING LOCATION: Desiccator Exhaust
SAMPLE TYPE: fec
RUN NUMBER: 100
OPERATOR: JCK
AMBIENT TEMPERATURE: 42
BAROMETRIC PRESSURE: 30.20
STATIC PRESSURE (P): 0.22
FALTER NUMBER IN: 111-27103
WATER FACTOR: .992

30.18

SCHEMATIC OF TRAVERSE POINT LAYOUT

Pre leak 0005 of 15

[illegible]

COMMENTS:

CPA-001275 38 M1

1914

FIELD DATA

PLANT Rocky Mount
 DATE 1-18-83
 SAMPLING LOCATION Incinerator Exhaust
 SAMPLE TYPE Particulate
 RUN NUMBER 4
 OPERATOR W. J. D.
 AMBIENT TEMPERATURE 43
 BAROMETRIC PRESSURE 30.22
 STATIC PRESSURE (in. Hg) 23.2
 FLOW METER NUMBER 117
 FLOW FACTOR 1.12

PROBE LENGTH AND TYPE 4' 5'
 NOZZLE I.D. 1/8"
 ASSUMED DENSITY 1.5
 SAMPLE BOX NUMBER 36
 METER BOX NUMBER 96
 METER AN 1.95
 C FACTOR 1.5
 PROBE HEATER SETTING 200
 HEATER RISE SETTING 300
 REFERENCE AQ 1.29

30.18

SCHEMATIC OF TRAVERSE POINT LAYOUT

Pre leak 000508 15.5 *Final leak 000808 15.0*

TRAVERSE POINT NUMBER	SAMPLING TIME, min	CLOCK TIME (in min)	GAS METER READING (ft ³ /min)	VELOCITY (ft/min)	ORIFICE PRESSURE (in. Hg)		STACK TEMPERATURE (°F)	OUTLET TEMPERATURE (°F)		PUMP VACUUM (in. Hg)	SAMPLE BOX TEMPERATURE (°F)	IMPERIAL TEMPERATURE (°F)
					DESIRED	ACTUAL		INLET	OUTLET			
A-1	5	15	570.31	128	2.7	2.7	98	62	62	3	240	36
2	10	20	574.90	134	3.3	3.3	99	70	62	5	240	39
3	15	25	579.94	140	3.9	3.9	98	78	62	6	227	40
4	20	30	584.95	139	3.8	3.8	99	82	64	6	235	42
5	25	35	590.60	151	4.8	4.8	98	86	66	8	249	42
6	30	40	597.100	165	6.2	6.2	99	88	66	10	241	44
START	30	44	597.100									
A-1	35	47	602.00	137	3.6	3.6	98	84	68	6	240	48
2	40	52	602.30	143	4.1	4.1	101	86	70	7	237	45
3	45	57	612.60	143	4.1	4.1	102	88	70	7	236	48
4	50	1502	618.30	155	5.3	5.3	97	92	72	9	245	50
5	55	07	624.15	156	5.3	5.3	97	92	72	9	245	50
6	60	12	630.059	156	5.3	5.3	99	92	72	9	241	50
	64		632.70				99.08	75	25			
			Depos. 68345.09									

Comments: 1. The end of the final leak check (in pump) early with the filter, about 5 min. after this operation. 2. During the leak test, the surface wind and wet & embedded as a ground surface.

71.6 m

FIELD DATA

PLANT Rocky Mount
 DATE 1-13-73
 SAMPLING LOCATION Intersect 12th St
 SAMPLE TYPE Gas
 RUN NUMBER 25
 OPERATOR MSK D3
 AMBIENT TEMPERATURE 45
 STATIC PRESSURE (in. H₂O) 30.30
 FILTER NUMBER (in) 113 20.73
 PROBE LENGTH AND TYPE 4' 55
 NOZZLE I.D. 0.310
 ASSUMED ORIFICE 5
 SAMPLE BOX NUMBER 912
 METER BOX NUMBER 912
 METER AN. 1.75
 C FACTOR 1.03
 PROBE HEATER SETTING 30
 HEATER BOX SETTING 250
 REFERENCE AN. 0.19

SCHEMATIC OF TRAVERSE POINT LAYOUT

Pre leak Rate 0.1 at 15" *Final leak Rate 0.1 at 15"*

TRAVERSE POINT NUMBER	CLOCK TIME (MIN:SEC)	GAS METER READING (ft ³)	VELOCITY HEAD (in. H ₂ O)	ORIFICE PRESSURE DIFFERENTIAL (in. H ₂ O)		STACK TEMPERATURE (°F)	DRY GAS METER TEMPERATURE (°F)		PUMP VACUUM (in. Hg)	SAMPLE BOX TEMPERATURE (°F)	INTEGRAL TEMPERATURE (°F)
				DESIRED	ACTUAL		INLET (°F)	OUTLET (°F)			
1	0:15:37	653.245	0.36	3.5	3.9	99	70	68	5	205	50
2	0:15:41	658.15	0.41	3.9	3.9	99	76	66	6	216	44
3	0:15:47	663.25	0.40	3.5	3.8	99	82	64	6	222	48
4	0:15:52	668.60	0.50	4.8	4.8	99	86	68	8	228	48
5	0:15:57	674.10	0.55	5.3	5.3	99	90	70	9	231	52
6	0:16:02	679.85	0.55	5.3	5.3	100	90	70	9	230	54
7	0:16:07	684.695									
8	0:16:10	686.695									
9	0:16:15	690.70	0.24	2.3	2.3	99	80	70	7	230	50
10	0:16:20	695.25	0.32	3.1	3.1	99	80	70	5	230	48
11	0:16:25	699.72	0.30	2.9	2.9	101	86	70	5	232	48
12	0:16:30	704.16	0.30	3.2	2.9	102	88	70	5	231	44
13	0:16:35	709.30	0.40	3.5	3.8	101	90	72	7	231	48
14	0:16:40	713.736	0.44	4.2	4.2	102	90	72	7	234	50
15	0:16:45						88	68			
16	0:16:50	60.490		3.82	3.82	99.92	70.67				
17	0:16:55	61.50									
18	0:17:00	63824.18									

COMMENTS
 EPA QM 25 64.0 ml.
 177

Plume Observation Record Form

DATA VALIDATION

R

DATE

Date 1/13/83

Observer David Savits

Checked By _____

Type of installation Storage

Twinister

Fuel _____ Stack Ht. _____

Observer's Distance from Stack

30' Ft.

Wind Speed 5-10 Direct _____

Sky Condition Clear

Plume Color Brown

Plume Background Blt

Plume Behavior _____

Steam Plume

detached _____ Ft. from stack

attached _____ Ft. dissipated

Start Time 0940

Ending Time 1043

Ending Weather Clear

Wind Speed 5-10 Direct _____

Sky Condition Clear

No. Units in Excess of
standard _____

5 min/hr. allow _____

No. Units of VIO. _____

Remarks:

Source Envirotech Co. River (Rocky Mount)

Address _____

Run # I

Sec.	0	15	30	45	Sec.	0	15	30	45
Min.					Min.				
0					30				
1					31				
2					32				
3					33				
4					34				
5					35				
6					36				
7					37				
8					38				
9					39				
10					0140	10	10	10	
11					41		10	0	
12					42	5	10	5	
13					43	5	5	5	
14					44		5	10	
15					45	5	10	5	
16					46	5	0	5	
17					47	10	15	15	
18					48		5	5	
19					49	5	5	5	
20					50	10	10	10	
21					51		5	5	
22					52		5	10	
23					53	10	10	10	
24					54	5	10	5	
25					55		20	20	
26					56		20	15	
27					57		10	10	
28					58		15	15	
29					59		15	15	

Plume Observation Record Form

DATA VALIDATION

BY

DATE

Date 1/13/83

Observer DW J. SQUILA

Checked By _____

Type of installation _____

Sludge Incinerator

Fuel _____ Stack Ht. _____

Observer's Distance from Stack

20 Ft.

Wind Speed 5 Direct _____

Sky Condition Clear

Plume Color _____

Plume Background _____

Plume Behavior _____

Steam Plume

detached _____ Ft. from stack

attached _____ Ft. dissipated

Start Time _____

Ending Time _____

Ending Weather _____

Wind Speed _____ Direct _____

Sky Condition _____

No. Units in Excess of
standard _____

5 min/hr. allow 20

No. Units of VIO. _____

Remarks:

0 = 4 = 0

5 = 132 = 660

10 = 78 = 780

15 = 27 = 405

20 = 7 = 140

248 1985

1985

248 = 8.00

Source Incinerator

Address TAG River

Wally Mount

Sec.	0	15	30	45	Sec.	0	15	30	45
Min.					Min.				
1	5	15	15	15	30	10	5	5	5
2	15	15	15	10	31	5	5	5	5
3	15	10	10	10	32	5	5	5	5
4	15	15	15	15	33	5	5	5	5
5	10	5	5	5	34	5	5	5	0
6	10	5	5	5	35	5	5	5	5
7	5	5	10	10	36	5	5	0	5
8	5	5	10	10	37	5	10	5	5
9	5	5	5	10	38	10	10	5	5
10	10	10	10	10	39	5	10	5	10
11					40	5	10	5	10
12					41	5	5	5	5
13	10	15	10	20	42	5	5	5	5
14	10	15	10	10	43	5	5	5	5
15	10	10	5	10	44				
16	10	5	10	5	45				
17	5	10	10	10	46				
18	5	5	10	10	47				
19	10	5	10	10	48				
20	5	10	5	5	49				
21	5	5	5	5	50				
22	5	5	10	5	51				
23	5	5	5	5	52				
24	5	5	5	5	53				
25	5	5	5	5	54				
26	5	5	5	5	55				
27	5	5	5	5	56				
28	5	5	10	10	57				
29	5	5	5	5	58				
					59				

Date 1/13/83Observer David S. S. S.Checked By Type of Installation Sludge IncineratorFuel Stack Ht. Observer Distance from Stack 20 Ft.Wind Speed 5-10 Direct Sky Condition B. ClearPlume Color BrownPlume Background BluePlume Behavior Steam Plume detached Ft. from stackattached Ft. dissipatedStart Time 1105Ending Time 1207Ending Weather ClearWind Speed 5-10 Direct Sky Condition Clear

No. Units in Excess of

standard 05 min/hr. allow 20No. Units of VIO. 0

Remarks:

0 = 5 = 05 - 167 = 83510 - 68 = 68015 - 8 = 12020 - 0 = 024816351635248 = 6.6

Plume Observation Record Form

DATA VALIDATION

BY DATE Source ExxonAddress The RiverRocky Mount N.C.Run # 2

Sec.	0	15	30	45	Sec.	0	15	30	45
Min.					Min.				
0	10	10	5	5	30	5	5	5	5
1	10	5	5	5	31	5	5	5	5
2	5				32	5	5	5	5
3					33	5	5	12	10
4					34	10	5	5	5
1105	10	10	5	5	35	5	5	5	5
6	10	5	5	5	36				
7	5	10	5	10	1127	5	5	5	5
8	10	5	5	5	38	5	5	5	5
9	5	5	5	5	39	5	5	5	5
20	5	5	5	5	40	10	10	10	10
21	5	5	10	10	41	5	10	10	5
22	10	10	10	5	42	10	5	5	5
23	5	5	5	5	43	5	5	5	5
24	5	5	5	5	44	5	5	5	5
25	5	10	5	5	45	5	5	5	10
26	5	10	10	5	46	5	5	5	10
27	5	5	10	5	47	10	10	5	10
28	5	0	5	5	48	5	10	5	5
29	5	5	5	0	49	10	15	10	5
30	5	10	5	5	50	10	5	10	10
31	5	10	5	5	51	5	10	5	5
32	5	10	5	5	52	5	5	5	5
33	5	10	5	5	53	5	10	5	5
34	5	5	5	5	54	5	5	5	5
35	5	10	5	5	55	5	10	5	5
36	5	10	5	10	56	5	5	5	10
37	5	5	5	5	57	5	5	10	10
38	5	5	5	5	58	10	5	10	5
39	5	5	5	5	59	10	5	5	5

REV. AQ-23 6/1/78

Date 1/13/83
 Observer Don S. Sina
 Checked By _____
 Type of installation Shady Tower

Fuel _____ Stack Ht. _____
 Observers Distance from Stack 20 Ft.
 Wind Speed 5 Direct _____
 Sky Condition Clear
 Plume Color Dark
 Plume Background Blue
 Plume Behavior _____

Steam Plume
 detached _____ Ft. from stack
 attached _____ Ft. dissipated

Start Time _____
 Ending Time _____
 Ending Weather _____
 Wind Speed _____ Direct _____
 Sky Condition _____

No. Units in Excess of
 standard _____
 5 min/hr. allow 20
 No. Units of VIO. _____

Remarks:

Plume Observation Record Form

Run # 12
 Source _____
 Address _____

DATA VALIDATION
 BY _____
 DATE _____

Sec.	0	15	30	45	Sec.	0	15	30	45
1	5	10	10	10	30				
2	5	5	5	5	31				
3	5	5	10	5	32				
4	5	10	10	5	33				
5	15	15	15	15	34				
6	10	10	10	10	35				
7	10	15	10	10	36				
8	5	5	10	15	37				
9					38				
10					39				
11					40				
12					41				
13					42				
14					43				
15					44				
16					45				
17					46				
18					47				
19					48				
20					49				
21					50				
22					51				
23					52				
24					53				
25					54				
26					55				
27					56				
28					57				
29					58				
					59				

Plume Observation Record Form

DATA VALIDATION

BY _____
DATE _____

Date 1-13-82

Observer David Soria

Checked By M.B.

Type of Installation _____

Shed Twinn

Fuel _____ Stack Ht. 10

Observers Distance from Stack

10 Ft.

Wind Speed 5 Direct N.E.

Sky Condition Clear

Plume Color Brown

Plume Background Brown

Plume Behavior _____

Steam Plume

detached _____ Ft. from stack

attached _____ Ft. dissipated

Start Time 1235

Ending Time 1336

Ending Weather Clear

Wind Speed 5-10 Direct _____

Sky Condition Clear

No. Units in Excess of
standard 0

5 min/hr. allow 20

No. Units of VIO. 0

Remarks:

Run 3

Source Enroute

Address Tar River

Rocky Mount N.C.

Run # III

Min.	0	15	30	45	Sec.	Min.	0	15	30	45
0	10	10			30					
1					31					
2					32					
3					33					
4					34					
5					35	10	10	10	10	10
6					36	5	5	5	5	5
7					37	10	10	10	10	10
8					38	10	10	10	10	10
9					39	5	5	5	5	5
10					40	5	5	5	5	5
11					41	5	5	5	5	5
12					42	5	5	5	5	5
13					43	10	10	10	10	10
14					44	5	5	5	5	5
15					45	10	10	10	10	10
16					46	5	5	5	5	5
17					47	10	10	10	10	10
18					48	10	10	10	10	10
19					49	5	5	5	5	5
20					50	10	10	10	10	10
21					51	5	5	5	5	5
22					52	10	10	10	10	10
23					53	5	5	5	5	5
24					54	5	5	5	5	5
25					55	5	10	15	15	15
26					56	15	15	15	15	15
27					57	15	15	15	15	15
28					58	10	10	10	10	10
29					59	15	10	15	15	15

Plume Observation Record Form

DATA VALIDATION

BY

DATE

Date 1/13/83

Observer David Sams

Checked By _____

Type of installation _____

Sludge Incinerator

Fuel _____ Stack Ht. _____

Observer's Distance from Stack

20 Ft.

Wind Speed 5 Direct _____

Sky Condition Clear

Plume Color Orange

Plume Background Blue

Plume Behavior _____

Steam Plume

detached _____ Ft. from stack

attached _____ Ft. dissipated

Start Time _____

Ending Time _____

Ending Weather _____

Wind Speed _____ Direct _____

Sky Condition _____

No. Units in Excess of
standard _____

5 min/hr. allow 20

No. Units of VIO. _____

Remarks:

REV. AQ-23 6/1/78

Source Environmental

Address Tai River

Rocky Mount

Run # 711

Sec.	0	15	30	45	Sec.	0	15	30	45
13:00	10	15	10	15	30	5	10	10	10
1	10	20	10	10	31	10	10	10	10
2	10	10	15	10	32	10	15	10	10
3	10	10	10	10	33	10	10	10	10
4	15	15	10	10	34	10	15	15	10
5	10	10	10	10	35	10	10	10	5
6					36	10	10	15	5
7	10	10	5	5	37				
8	5	10	5	5	38				
9	5	5	5	10	39				
10	5	5	5	5	40				
11	5	5	5	5	41				
12	5	10	10	5	42				
13	5	10	10	10	43				
14	15	20	15	10	44				
15	10	5	5	10	45				
16	10	10	5	10	46				
17	10	5	5	5	47				
18	5	10	10	10	48				
19	10	15	10	10	49				
20	10	10	15	15	50				
21	10	10	10	15	51				
22	15	10	10	10	52				
23	10	10	10	10	53				
24	5	10	10	5	54				
25	10	10	5	10	55				
26	5	10	15	15	56				
27	10	10	15	10	57				
28	15	10	10	10	58				
29	10	10	10	10	59				

Plume Observation Record Form

DATA VALIDATION
BY _____
DATE _____

Date 1/13/53

Observer Paul Sams

Checked By _____

Type of installation _____

Shelby Incinerator

Fuel _____ Stack Ht. _____

Observer's Distance from Stack

20 Ft.

Wind Speed 5 Direct _____

Sky Condition Clear

Plume Color Black

Plume Background _____

Plume Behavior _____

Steam Plume

detached _____ Ft. from stack

attached _____ Ft. dissipated

Start Time 1410

Ending Time 1512

Ending Weather _____

Wind Speed _____ Direct _____

Sky Condition _____

No. Units in Excess of
standard _____

5 min/hr. allow 20

No. Units of VIO. _____

Remarks:

0 = 4 - 0

5 = 121 = 670

10 = 1.5 = 1050

15 = " = 135

20 = 0 = 0

252 1855

1855

252 = 7.4

Source Envirocheck

Address Tac River

Rocky Mount N.C.

2.4

Sec.	0	15	30	45	Sec.	0	15	30	45
Min.					Min.				
1500	10	5	5	10	30				
1	5	0	5	5	31				
2	0	10	5	5	32				
3	10	5	5	5	33				
4	5	5	10	5	34				
5	5	5	5	5	35				
6	5	5	5	10	36				
7	10	5	5	10	37				
8	10	10	5	5	38				
9	5	5	10	10	39				
10	5	5	5	0	40				
11	2	10	5	10	41				
12	10	5	5	10	42				
13					43				
14					44				
15					45				
16					46				
17					47				
18					48				
19					49				
20					50				
21					51				
22					52				
23					53				
24					54				
25					55				
26					56				
27					57				
28					58				
29					59				

Date 1/13/53
 Observer Davis/Kane
 Checked By _____
 Type of Installation _____
Sludge Incinerator

Fuel _____ Stack Ht. _____
 Observers Distance from Stack
20 Ft.

Wind Speed 5-10 Direct _____

Sky Condition Clear

Plume Color Brown

Plume Background Blue

Plume Behavior _____

Steam Plume
 detached _____ Ft. from stack
 attached _____ Ft. dissipated

Start Time 1537

Ending Time 1640

Ending Weather Clear

Wind Speed 5-10 Direct _____

Sky Condition Clear

No. Units in Excess of
 standard 0

5 min/hr. allow 20

No. Units of VIO. 0

Remarks:

0 = 0 = 0

5 = 72 = 360

10 = 153 = 1,530

15 = 19 = 285

20 = 0 = 0

244 2175

2175

244 = 8.9

Plume Observation Record Form

Source Envirotech
 Address Tax River
Rocky Mount

DATA VALIDATION
 BY _____
 DATE _____

Run # IV

Sec.	0	15	30	45	Sec.	0	15	30	45
Min.					Min.				
0	5	5	5	5	30				
1	5	10	5	5	31				
2	10				32				
3					33				
4					34				
5					35				
6					36				
7					37	5	5	5	5
8					38	5	10	5	5
9					39	10	5	10	5
10					40	5	5	10	5
11					41	5	5	5	5
12					42	5	10	5	5
13					43	10	10	15	10
14					44	10	10	10	5
15					45	5	10	10	10
16					46	10	5	5	10
17					47	10	5	10	10
18					48	5	10	5	5
19					49	5	5	5	5
20					50	5	10	10	5
21					51	5	10	10	5
22					52	10	10	5	10
23					53	10	5	10	5
24					54	5	5	10	10
25					55	10	5	10	10
26					56	5	5	5	5
27					57	10	10	15	15
28					58	10	10	10	10
29					59	10	10	10	10

DATA VALIDATION

52

DATE _____

Date 1-13-83

Observer D. O. Smith

Checked By _____

Type of installation

Shiloh Zwierlein

Fuel _____ Stock No. _____

Observers Distance from Stack

30 ft.

Wind Speed 5-10 Direct

Sky Condition Clear

Plume Color Brown

Plume Background Line

Flame Behavior

Steam Plans

detached _____ Ft. from stack

attached _____ Ft. dissipated

Start Time 1537

Ending Time 1640

Ending Weather

Wind Speed 510 Direct

Sky Condition *C*

12. *Journal of the American Medical Association*, 273:1225-1226 (1995).

NO. UNITS IN EXCESS OF

3 MIN/HR. ALLOW 20

NO. DATES OF VIS.

Remarks :

Source Envestech

Address Tar River

Beck, Maud

~~2. 10~~

Sec.					Sec.				
Nin.	0	25	50	75	Nin.	0	25	50	75
1600	10	10	10	10	30	10	5	5	10
1	10	10	15	10	31	5	5	10	5
2	10	10	10	15	32	10	10	10	10
3	10	10	10	10	33	5	10	10	10
4	10	10	10	10	34	5	10	10	10
5	10	10	10	10	35	5	10	10	10
6	10	10	10	15	36	10	10	10	5
7	10	10	10	15	37	5	10	15	15
8					38	15	10	10	10
9					39	10	10	10	10
10	10	10	15	10	40				
11	10	15	10	15	41				
12	10	10	10	10	42				
13	10	5	5	10	43				
14	10	10	10	10	44				
15	10	10	10	10	45				
16	10	10	15	15	46				
17	10	10	10	15	47				
18	10	10	10	10	48				
19	15	15	10	10	49				
20	10	10	10	10	50				
21	10	5	10	5	51				
22	10	5	5	10	52				
23	10	10	5	5	53				
24	10	10	5	5	54				
25	5	5	5	5	55				
26	10	10	10	5	56				
27	10	10	10	10	57				
28	10	10	5	15	58				
29	10	10	5	10	59				

REV. AQ-23 6/1/78

**FEED RATE CHECK — CONVEYOR TO TARED TRUCK
WHICH WAS WATCHED AFTER EACH TEST RUN**

SAMPLE ORDER	BELT SPEED %	TIME OF RUN	WEIGHT OF RUN	EQUIVALENT LBS/HOUR
4	30	30 MIN	2220	4440
2	40	30 MIN	2940	5880
3	50	30 MIN	3000	6000
1	60	30 MIN	4820	9640

8480

NORTH CAROLINA
PUBLIC WEIGHMASTER
LICENSE EXPIRES JUNE 30, 1963
Mary Jo-Ann Burnette 9563
Mary Jo-Ann Burnette
WALD UNLESS NOTED
4440 30%

TRUCK TARE

110700
8480
2220

NORTH CAROLINA
PUBLIC WEIGHMASTER
LICENSE EXPIRES JUNE 30, 1963
Mary Jo-Ann Burnette 9563
Mary Jo-Ann Burnette
WALD UNLESS NOTED

30%

5720 / HR

111420
8480
2940

40%
NORTH CAROLINA
PUBLIC WEIGHMASTER
LICENSE EXPIRES JUNE 30, 1963
Mary Jo-Ann Burnette 9563
Mary Jo-Ann Burnette
WALD UNLESS NOTED

40%

11480
8480
3000 26000

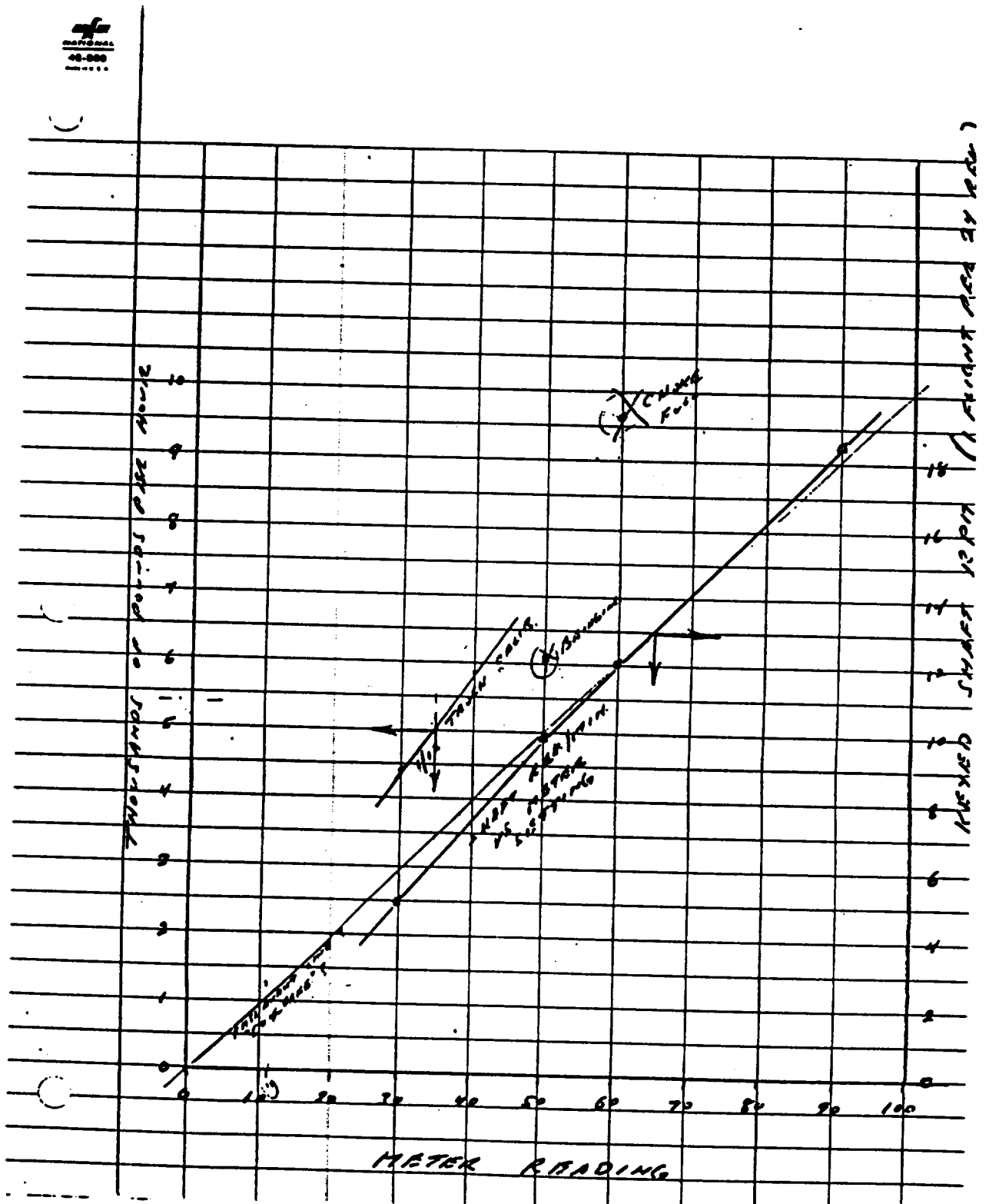
50%
NORTH CAROLINA
PUBLIC WEIGHMASTER
LICENSE EXPIRES JUNE 30, 1963
Mary Jo-Ann Burnette 9563
Mary Jo-Ann Burnette
WALD UNLESS NOTED

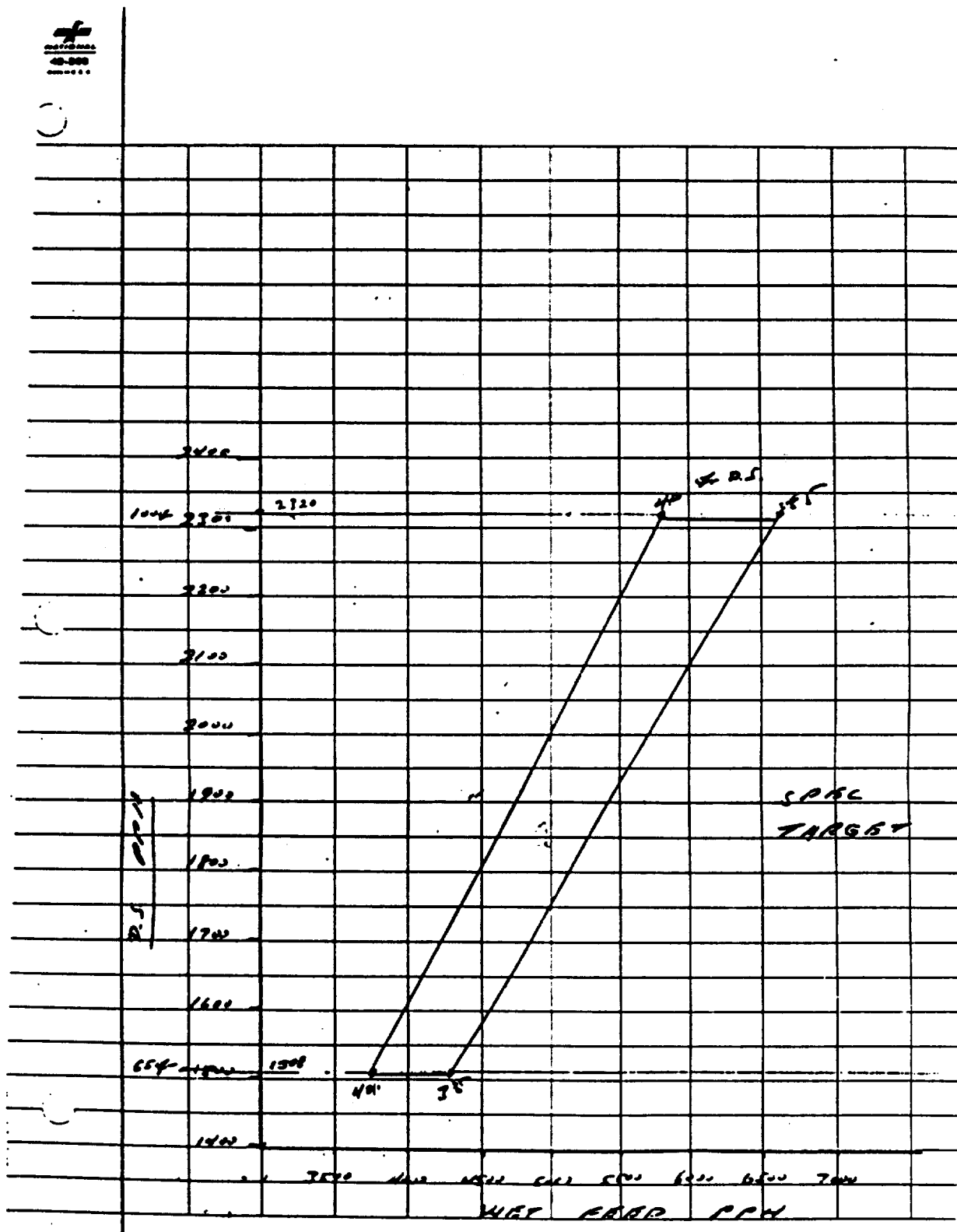
50%

113300
8480
4820

60%
NORTH CAROLINA
PUBLIC WEIGHMASTER
LICENSE EXPIRES JUNE 30, 1963
Mary Jo-Ann Burnette 9563
Mary Jo-Ann Burnette
WALD UNLESS NOTED

60%





SHEET I
 SHEET II
 SHEET III
 Date 11/13/93

Rocky 17T

TEMPS.										SCANNER SYSTEM										RUBBER STAMP	
1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22
0000	000	100	145	170	185	195	200	205	210	215	220	225	230	235	240	245	250	255	260	265	270
0100	005	105	145	170	185	195	200	205	210	215	220	225	230	235	240	245	250	255	260	265	270
0200	010	110	145	170	185	195	200	205	210	215	220	225	230	235	240	245	250	255	260	265	270
0300	015	115	145	170	185	195	200	205	210	215	220	225	230	235	240	245	250	255	260	265	270
0400	020	120	145	170	185	195	200	205	210	215	220	225	230	235	240	245	250	255	260	265	270
0500	025	125	145	170	185	195	200	205	210	215	220	225	230	235	240	245	250	255	260	265	270
0600	030	130	145	170	185	195	200	205	210	215	220	225	230	235	240	245	250	255	260	265	270
0700	035	135	145	170	185	195	200	205	210	215	220	225	230	235	240	245	250	255	260	265	270
0800	040	140	145	170	185	195	200	205	210	215	220	225	230	235	240	245	250	255	260	265	270
0900	045	145	145	170	185	195	200	205	210	215	220	225	230	235	240	245	250	255	260	265	270
1000	050	150	145	170	185	195	200	205	210	215	220	225	230	235	240	245	250	255	260	265	270
1100	055	155	145	170	185	195	200	205	210	215	220	225	230	235	240	245	250	255	260	265	270
1200	060	160	145	170	185	195	200	205	210	215	220	225	230	235	240	245	250	255	260	265	270
1300	065	165	145	170	185	195	200	205	210	215	220	225	230	235	240	245	250	255	260	265	270
1400	070	170	145	170	185	195	200	205	210	215	220	225	230	235	240	245	250	255	260	265	270
1500	075	175	145	170	185	195	200	205	210	215	220	225	230	235	240	245	250	255	260	265	270
1600	080	180	145	170	185	195	200	205	210	215	220	225	230	235	240	245	250	255	260	265	270
1700	085	185	145	170	185	195	200	205	210	215	220	225	230	235	240	245	250	255	260	265	270
1800	090	190	145	170	185	195	200	205	210	215	220	225	230	235	240	245	250	255	260	265	270
1900	095	195	145	170	185	195	200	205	210	215	220	225	230	235	240	245	250	255	260	265	270
2000	100	200	145	170	185	195	200	205	210	215	220	225	230	235	240	245	250	255	260	265	270
2100	105	205	145	170	185	195	200	205	210	215	220	225	230	235	240	245	250	255	260	265	270
2200	110	210	145	170	185	195	200	205	210	215	220	225	230	235	240	245	250	255	260	265	270
2300	115	215	145	170	185	195	200	205	210	215	220	225	230	235	240	245	250	255	260	265	270

APPENDIX C
FIELD ANALYTICAL DATA SHEETS

TRW

ANALYTICAL DATA

PLANT Rocky Mount
DATE 1-13-83
SAMPLING LOCATION Incinerator Exhaust
SAMPLE TYPE Part
RUN NUMBER 1
SAMPLE BOX NUMBER 9E
CLEAN-UP MAN MCA

COMMENTS:

FRONT HALF Invalid

LABORATORY RESULTS

ACETONE WASH OF NOZZLE, PROBE, CYCLONE (BYPASS),
FLASK, FRONT HALF OF FILTER HOLDER

CONTAINER _____

FILTER NUMBER 110

CONTAINER _____

FRONT HALF SUBTOTAL _____

BACK HALF

IMPINGERS CONTENTS AND WATER WASH OF
IMPINGERS, CONNECTORS, AND BACK
HALF OF FILTER HOLDER

CONTAINER _____
ETHER-CHLOROFORM
EXTRACTION _____

ACETONE WASH OF IMPINGERS, CONNECTORS,
AND BACK HALF OF FILTER HOLDER

CONTAINER _____

BACK HALF SUBTOTAL _____

TOTAL WEIGHT _____

MOISTURE

IMPINGERS
FINAL VOLUME _____ ml
INITIAL VOLUME 200 ml
NET VOLUME _____ ml

SILICA GEL
FINAL WEIGHT _____ g
INITIAL WEIGHT 200 g
NET WEIGHT _____ g

TOTAL MOISTURE _____ %

EPA (Dwt) 231
4/72

TRW

ANALYTICAL DATA

PLANT Rocky Mount
DATE 1-13-83
SAMPLING LOCATION Incinerator Exhaust
SAMPLE TYPE Part
RUN NUMBER Run #2
SAMPLE BOX NUMBER _____
CLEAN-UP MAN MR DS

COMMENTS:

FRONT HALF

ACETONE WASH OF NOZZLE, PROBE, CYCLONE (BYPASS),
FLASK, FRONT HALF OF FILTER HOLDER

FILTER NUMBER # 112

LABORATORY RESULTS

CONTAINER 4618

20.0 mg

CONTAINER 4623

47.6 mg

FRONT HALF SUBTOTAL 67.6 mg

BACK HALF

IMPINGER CONTENTS AND WATER WASH OF
IMPINGERS, CONNECTORS, AND BACK
HALF OF FILTER HOLDER

CONTAINER _____
ETHER-CHLOROFORM
EXTRACTION

ACETONE WASH OF IMPINGERS, CONNECTORS,
AND BACK HALF OF FILTER HOLDER

CONTAINER _____

BACK HALF SUBTOTAL _____ mg

TOTAL WEIGHT 67.6 mg

MOISTURE

IMPINGERS

FINAL VOLUME 220.0 ml
INITIAL VOLUME 200.0 ml
NET VOLUME 20.0 ml

SILICA GEL

FINAL WEIGHT 210.6 g 251.15 g
INITIAL WEIGHT 200.11 g 200.0 g
NET WEIGHT 10.49 g 51.15 g

TOTAL MOISTURE 21.5 %

EPA (Dwt) 231
4/72

TRW

ANALYTICAL DATA

PLANT Rocky Mount
DATE 1-13-83
SAMPLING LOCATION Incinerator Exhaust
SAMPLE TYPE Part.
RUN NUMBER Run # 3
SAMPLE BOX NUMBER _____
CLEAN-UP MAN MR PS

COMMENTS:

FRONT HALF

LABORATORY RESULTS

ACETONE WASH OF NOZZLE, PROBE, CYCLONE (BYPASS),
FLASK, FRONT HALF OF FILTER HOLDER

CONTAINER 4619

5.3 mg

FILTER NUMBER 111

CONTAINER 4624

48.1 mg

FRONT HALF SUBTOTAL 53.4 mg

BACK HALF

IMPINGER CONTENTS AND WATER WASH OF
IMPINGERS, CONNECTORS, AND BACK
HALF OF FILTER HOLDER

CONTAINER _____
ETHER-CHLOROFORM
EXTRACTION

mg

mg

ACETONE WASH OF IMPINGERS, CONNECTORS,
AND BACK HALF OF FILTER HOLDER

CONTAINER _____

mg

BACK HALF SUBTOTAL _____ mg

TOTAL WEIGHT _____ mg

MOISTURE

IMPINGERS

FINAL VOLUME 223 ml

INITIAL VOLUME 200 ml

NET VOLUME 23 ml

SILICA GEL

FINAL WEIGHT 916 g

INITIAL WEIGHT 900 g

NET WEIGHT 16 g

TOTAL MOISTURE 35 g

EPA (Dev) 231

4/72

TRW

ANALYTICAL DATA

PLANT Rocky Mount
DATE 1-13-83
SAMPLING LOCATION Incinerator Exhaust
SAMPLE TYPE Particulate
RUN NUMBER Run #4
SAMPLE BOX NUMBER _____
CLEAN-UP MAN McB D.S.

COMMENTS:

Fifteen Back Flush
at End of Test

FRONT HALF

ACETONE WASH OF NOZZLE, PROBE, CYCLONE (BYPASS),
FLASK, FRONT HALF OF FILTER HOLDER

CONTAINER 4620
4622

LABORATORY RESULTS

26.3
46.9

FILTER NUMBER

117

CONTAINER 4625

6.1

FRONT HALF SUBTOTAL 79.3

BACK HALF

IMPINGERS CONTENTS AND WATER WASH OF
IMPINGERS, CONNECTORS, AND BACK
HALF OF FILTER HOLDER

CONTAINER _____
ETHER-CHLOROFORM
EXTRACTION _____

ACETONE WASH OF IMPINGERS, CONNECTORS,
AND BACK HALF OF FILTER HOLDER

CONTAINER _____

BACK HALF SUBTOTAL _____

TOTAL WEIGHT 79.3

MOISTURE

IMPINGERS 211.9
FINAL VOLUME 200 ml
INITIAL VOLUME 200 ml
NET VOLUME 11.9 ml

SILICA GEL
FINAL WEIGHT 259.7 g
INITIAL WEIGHT 200.0 g
NET WEIGHT 59.7 g

TOTAL MOISTURE 71.6 g

EPA (Dwt) 231
4/72

TRW

ANALYTICAL DATA

PLANT Envirotech Rocky Mount
DATE 1/13/93
SAMPLING LOCATION Incinerator Exhaust
SAMPLE TYPE Particulate
RUN NUMBER Run # 5
SAMPLE BOX NUMBER # 5
CLEAN-UP MAN D. SAVIA

COMMENTS:

FRONT HALF

ACETONE WASH OF NOZZLE, PROBE, CYCLONE (BYPASS),
FLASK, FRONT HALF OF FILTER HOLDER

FILTER NUMBER 113

LABORATORY RESULTS

CONTAINER 4621 8.2 mg

CONTAINER 4626 38.8 mg

FRONT HALF SUBTOTAL 47.0 mg

BACK HALF

IMPINGERS CONTENTS AND WATER WASH OF
IMPINGERS, CONNECTORS, AND BACK
HALF OF FILTER HOLDER

ACETONE WASH OF IMPINGERS, CONNECTORS,
AND BACK HALF OF FILTER HOLDER

CONTAINER _____ mg
ETHER-CHLOROFORM
EXTRACTION _____ mg

CONTAINER _____ mg

BACK HALF SUBTOTAL _____ mg

TOTAL WEIGHT 47.0 mg

MOISTURE

IMPINGERS
FINAL VOLUME 232 ml
INITIAL VOLUME 200 ml
NET VOLUME 32 ml

SILICA GEL
FINAL WEIGHT 232 g _____ g
INITIAL WEIGHT 200 g _____ g
NET WEIGHT 32 g _____ g

EPA (Dwt) 231
472

TOTAL MOISTURE 64.0 %

WORK SHEET

Proc. Manual
G.C. Form 173

	Rev. 2	3	3	3	4	4	5	5
CO ₂	30	30	32	32	40.5	41	46.4	5
O ₂	52.5	52.5	50.5	51	46.5	46.5	53.5	22.5
N ₂	56	56	56	56	56	56	56	54
2 CO ₂	4.92			5.25				56
2 O ₂	15.89		15.36		6.68			56
Sum Cal. Gas	79.19		79.39		14.08			4.51
CO ₂ 17.87%	83.5	86.4			79.24			16.27
O ₂ 7.07%	27	56.4						79.22
N ₂ 78.13%	56	112.8						
Cal. Gas #35								
CO ₂ 2.88%	12.5	86.4						
O ₂ 16.87%	55.5	86.4						
N ₂ 80.32%	56.5	112.5						
Cal. Gas #10								
CO ₂ 15.6	86	86.4						
O ₂ 5.08	19.5	86.4						
N ₂ 72.32	53.5	112.8						
CO 7.00	61	86.4						

bound on Max 35

used for 11/1/49

CALCULATED FEED RATE FROM TRW ANALYSES

ITEM			TEST			DATA SOURCE	
LINE NO.		ITEM UNITS	TEST TIME AVE.	2	3	5	(N) INDICATES LINE NUMBER
11							
2	STACK FLOW	DSCFM		3916	4120	4488	TRW
3							
4	CO ₂	% D.B.		4.92	5.25	4.51	TRW
5							
6	CO ₂	70°F DSCFM		192.7	216.3	202.4	(2) x (4)
7							
8	CO ₂	PPH		1321	1483	1388	(6) x $\frac{60}{355}$ x 44 ∴ (6) x 6.86
9							
10	FUEL	GPH		4	6.5	8.0	LOG SHEET
11	FUEL	PPH		28.3	46.0	56.6	7.0% #/GAL.
12	FUEL CARBON	PPH		24.4	39.7	48.7	TRW ANALYSIS ∴ 0.861 x (11)
13							
14	FUEL CO ₂	PPH		90	146	179	(12) x $\frac{44}{12}$ ∴ 3.67 x (12)
15							
16	CO ₂ FEED VOL.	PPH	1259	1231	1337	1209	(8) - (14)
17							(PPH x 5) (CARBON x $\frac{44}{12}$) = CARBON FEED VOL
18	FEED VOL.	PPH	798	780	847	766	∴ FEED VOL = (16) / 1.578
19							
20	FEED VOL	% D.B.	59.9	59.9	59.9	59.9	59.75 + 60.0 TRW ANALYSIS
21							
22	FEED D.S.	PPH	1332	1302	1414	1279	(18) ÷ (20)
23							
24	FEED D.S.	% W.B.	32.3	33	32	32	TRW ANALYSIS
25							
26	TOTAL WET FEED	PPH	4124	3916	4419	3997	(22) ÷ $\frac{24}{100}$
27							
28							

TRW

PROJECT Environtech Rocky Mount

A	B	C	D	E	F	G	H	J	K
Sample #	Container #	Time	Wet Gross	Tare	Wet Gross - Tare	Dry Gross	Tare	Dry Gross - Tare	% Moisture
4590	1	8:00A	25.2321	1.5400	23.6921	9.6347	1.5400	8.0947	34
4591	2	8:30	25.2325	1.5287	23.7038	8.8505	1.5287	7.1751	32
4592	3	9:00	25.2365	1.5286	23.7079	9.0413	1.5286	7.4627	32
4593	4	9:30	25.2375	1.5284	23.7091	9.2728	1.5284	7.7244	31
4594	5	10:00	25.2380	1.5283	23.7097	9.4814	1.5283	7.9241	33
4595	6	10:30	25.2406	1.5493	23.6913	8.6037	1.5493	7.0524	30
4596	7	11:00	25.2457	1.5479	23.6978	9.3168	1.5479	7.6689	33
4597	8	11:30	25.2316	1.5535	23.6781	9.2036	1.5535	7.1481	34
4598	9	12:00	25.2471	1.5485	23.6986	9.4994	1.5485	7.9509	33
4599	10	12:30	25.2425	1.5534	23.6891	9.5304	1.5534	7.9719	33

L	M	N	P	O	R	S
Blank	Container #	Volume	Gross - Tare Net			Blank Wt

Date Jan. 18, 1983
Analyst David Savia
Wt Units Grams

NOTE:

TRW

PROJECT Enrichment Rocky Mount

A	B	C	D	E	F	G	H	J	K
Sample #	Container #	Time	Wet Gross	Tare	U/Gross - Tare	Dry Gross	Tare	Dry Gross - Tare	Wet/Dry % Moisture
4600	11	1300	25.5817	1.5519	24.0298	9.1911	1.5519	7.6392	32
4601	12	1330	25.5019	1.5414	23.9605	8.7983	1.5414	7.2569	30
4602	13	1400	24.9688	1.5467	23.4221	9.0784	1.5467	7.5017	32
4603	14	1430	25.5142	1.5444	23.9698	9.7596	1.5444	8.2152	34
4604	15	1500	26.2976	1.5176	24.7800	9.4393	1.5176	7.8917	32
4605	16	1530	27.3018	1.5417	25.7601	9.4677	1.5417	7.9260	31
4606	17	1600	27.2597	1.5527	25.7070	8.9838	1.5527	7.1311	33
4607	18	1630	25.0160	1.5458	23.4702	9.4036	1.5158	7.8568	33
4608	19	1645	25.4982	1.5515	23.9467	8.9558	1.5515	7.4073	31
4609	20	Composite	24.3984	1.5533	22.8451	8.8116	1.5533	7.2583	32

L	M	N	P	O	R	S
Blank	Container #	Volume	Gross - Tare Net	Orig. wt.	Final Wt.	Blank Wt Gain
Blank						
Blank	21			1.5401	1.5401	00.00

Date Jan 18, 1983
 Analyst David Soria
 Wt Units Grams

NOTE:

TRW

PROJECT Envirotech Becky Mount

A	B	C	D	E	F	G	H	J	K
Sample #	Container #	Sample Volume	Aliquot	Gross	Tare	Net			
Run #2	4623			0.7559	0.7083	0.0476			
Run #3	4624			0.7494	0.7013	0.0481			
Run #4	4625			0.7020	0.7009	0.0061			
Run #5	4626			0.7761	0.7073	0.0388			
Run #2	4618	175		155.1673	155.1472	0.0200			
Run #3	4619	160		154.0734	154.0674	0.0053			
Run #4	4620	325		155.3791	155.3525	0.0263			
Run #4	4622	250		155.5552	155.5033	0.0469			
Run #5	4621	171		154.2704	154.2622	0.0052			

Films

Beckman

L	M	N	P	Q	R	S
Blank	Container #	Volume	Gross - Tare Net	Gross	Tare	Blank Wt
Asstons	4627	100ML		156.0961	156.0367	-0.0006

Date 1-18-82
 Analyst D.S. MCR
 Wt Units grams

NOTE:

APPENDIX E
METER BOX CALIBRATION SHEETS

DRY GAS METER CALIBRATION DATA

(English Units)

Pretest ☒ Post Test ☐

Date 12/9/82

Barometric Pressure, Bp = 30.19

Meter Box # 9E

Dry Gas Meter # 523600

Orifice manometer setting, ΔH, in. H ₂ O	Manometer Pressure Of Wet Test Meter ΔH	Gas volume wet test meter V _w , ft ³	Gas volume dry gas meter V _d , ft ³	Temperature				Time H, Min. .00	γ	ΔHQ		
				Wet test Meter t _w , °F	Dry gas meter							
					Inlet t _{di} , °F	Outlet t _{do} , °F	Average t _d , °F					
1.5	2.0	4.998 0 4.998	4.63.300 958.300 5.000	71	73 74 74	81 82 82	87.5	13.20	1.00	1.87		
1.0	2.3	10.000 0 10.000	973.395 963.000 972.395	71	83 72 74 74	82 84 84 85	87.8	19.1	.984	1.92		
2.0	2.65	10.500 0 10.500	994.775 973.395 10.720	71	86 80 78 78	82 84 84 82	88.0	14.27	.999	1.98		
3.0	3.4	10.003 0 10.003	994.690 984.465 10.175	71	86 72 90 120	83 84 84 85	89.25	11.27	1.00	2.05		
										ΔHQ Avg.	1.001	1.95

$$\frac{V_w \left(P_b - \frac{\Delta H_w}{13.6} \right) (t_d + 460)}{V_d \left(P_b + \frac{\Delta H_w}{13.6} \right) (t_w + 460)}$$

$$\frac{0.0317 \Delta H}{P_b (t_d + 460)} \left[\frac{t_w + 460}{V_w} \right]^2$$

$\frac{4.998 \times 30.04 \times 547.5}{5.000 \times 30.02 \times 531.0} = 1.02$	$.00000955 [1966728.284] = 1.87$
$\frac{10.000 \times 30.02 \times 547.8}{10.395 \times 30.06 \times 531.0} = .994$	$.000001774 \times 1023621.424 = 1.92$
$\frac{10.500 \times 30.00 \times 548}{10.720 \times 30.34 \times 531} = .999$	$.000003807 \times 520284.899 = 1.98$
$\frac{10.003 \times 29.94 \times 549.25}{10.175 \times 30.41 \times 531} = 1.001$	$.000005735 \times 358718.063 = 2.05$

γ = Ratio of accuracy of wet test meter to dry test meter. Tolerance = ±0.01.
 ΔH = Orifice pressure differential that gives 0.75 cfm of air at 70°F and 29.92 inches of mercury, in. H₂O. Tolerance = ±0.15.

Post test tolerance must be within ± 0.05 and within a range of 0.10

Meter Leak Check Front ☒ Back ☒

Pitot Leak Check ☒

Electrical Check ☒

Remarks

Calibrating technician DBJ

DRY GAS METER CALIBRATION DATA (English Units)

Pretest ☐ Post Test ☒

Date 1/25/93

Barometric Pressure, Bp = 29.87

Meter Box # 9E

Dry Gas Meter # _____

Orifice manometer setting, ΔH, in. H ₂ O	Manometer Pressure Of Wet Test Meter Δ HW	Gas volume wet test meter V _w , ft ³	Gas volume dry gas meter V _d , ft ³	Temperature				Time N. Min. .00	Y	ΔHQ
				Wet test	Dry gas meter					
					Meter t _w , °F	Inlet t _{di} , °F	Outlet t _{do} , °F			
2.0	-2.6	10.500	757.790 746.400 11.190	63.0	108 112	90 94	101		.997	
2.0	-2.6	11.0	769.565 757.790 11.775	63.0	112 113	94 96 97	105.6		.998	

Y

ΔHQ Avg.

$$\frac{V_w \left(P_b - \frac{\Delta H_w}{13.6} \right) (t_d + 460)}{V_d \left(P_b + \frac{\Delta H_w}{13.6} \right) (t_w + 460)}$$

$$\frac{0.0317 \Delta H}{P_b (t_d + 460)} \left[\frac{t_w + 460}{t_w} \right]^2$$

10.500 x 29.67 x 561 = .994	
11.190 x 30.02 x 523	
x 29.67 x 565.6	
11.775 x 30.02 x 523 = .998	

Y = Ratio of accuracy of wet test meter to dry test meter. Tolerance = ±0.01.
ΔH@ = Orifice pressure differential that gives 0.75 cfm of air at 70°F and 29.92 inches of mercury, in. H₂O. Tolerance = ±0.15.
Post test tolerance must be within ± 0.05 and within a range of 0.10

Meter Leak Check Front ☒ Back ☒

Pitot Leak Check ☒

Electrical Check ☒

Remarks

Calibrating technician DBS

APPENDIX F

PERSONNEL

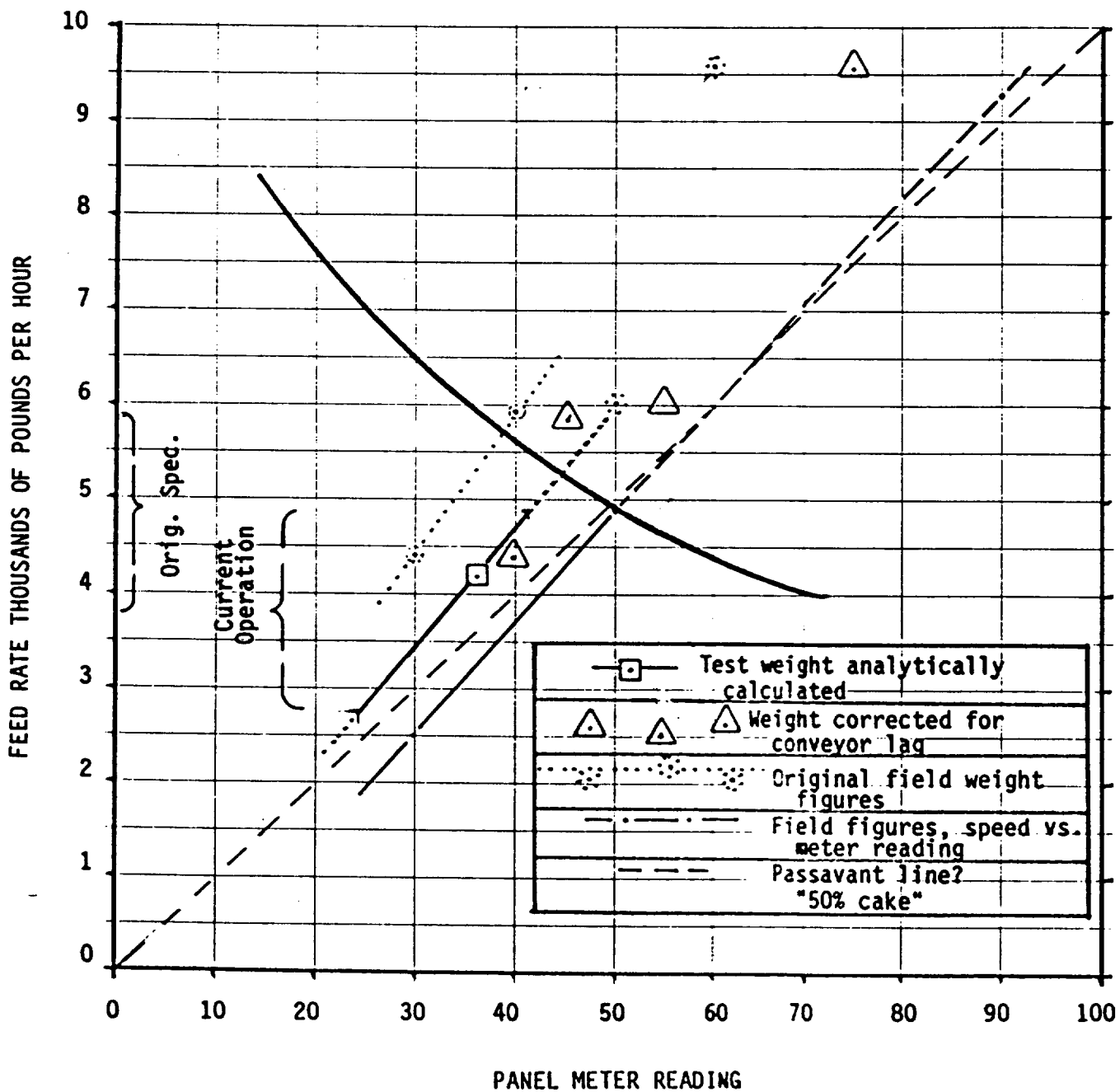
PERSONNEL

1. Mr. E. Fuller State of North Carolina
2. J. McReynolds TRW
3. D. Savia TRW

APPENDIX G
REPORT SUPPLEMENT BY OTHERS

CALCULATED FEED RATE FROM TRW ANALYSES

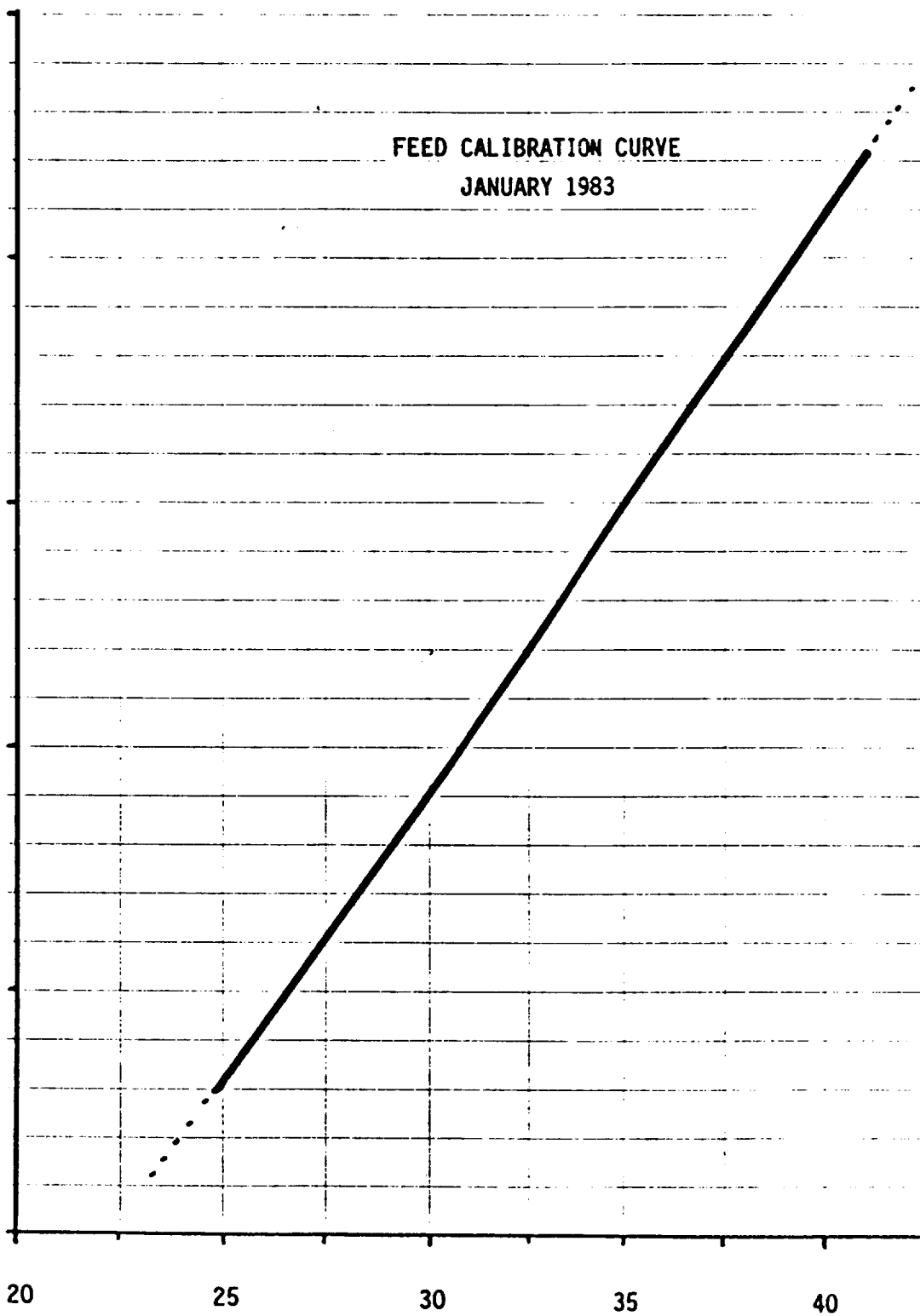
ITEM			TEST			DATA SOURCE	
LINE NO.		ITEM UNITS	TEST TIME AVE.	2	3	5	(N) INDICATES LINE NUMBER
11							
2	STACK FLOW	DSCFM		3916	4120	4488	TRW
3							
4	CO ₂	% D.B.		4.92	5.25	4.51	TRW
5							
6	CO ₂	70°F DSCFM		192.7	216.3	202.4	(2) x (4)
7							
8	CO ₂	PPH		1321	1483	1388	(6) x $\frac{60}{355}$ x 44 ∴ (6) x 6.86
9							
10	FUEL	GPH		4	6.5	8.0	LOG SHEET
11	FUEL	PPH		28.3	46.0	56.6	7.0% #/GAL.
12	FUEL CARBON	PPH		24.4	39.7	48.7	TRW ANALYSIS ∴ 0.861 x (11)
13							
14	FUEL CO ₂	PPH		90	146	179	(12) x $\frac{44}{12}$ ∴ 3.67 x (12)
15							
16	CO ₂ FEED VOL.	PPH	1259	1231	1337	1209	(8) - (14)
17							(PPH x 5) (CARB. F. $\frac{44}{12}$) = CARBON FROM FEED VOL.
18	FEED VOL.	PPH	798	780	847	766	∴ FEED VOL = (16) / 1.578
19							
20	FEED VOL	% D.B.	59.9	59.9	59.9	59.9	59.75 + 60.0 TRW ANALYSIS
21							
22	FEED D.S.	PPH	1332	1302	1414	1279	(18) ÷ (20)
23							
24	FEED D.S.	% W.B.	32.3	33	32	32	TRW ANALYSIS
25							
26	TOTAL WET FEED	PPH	4124	3916	4419	3997	(22) ÷ $\frac{24}{100}$
27							
28							



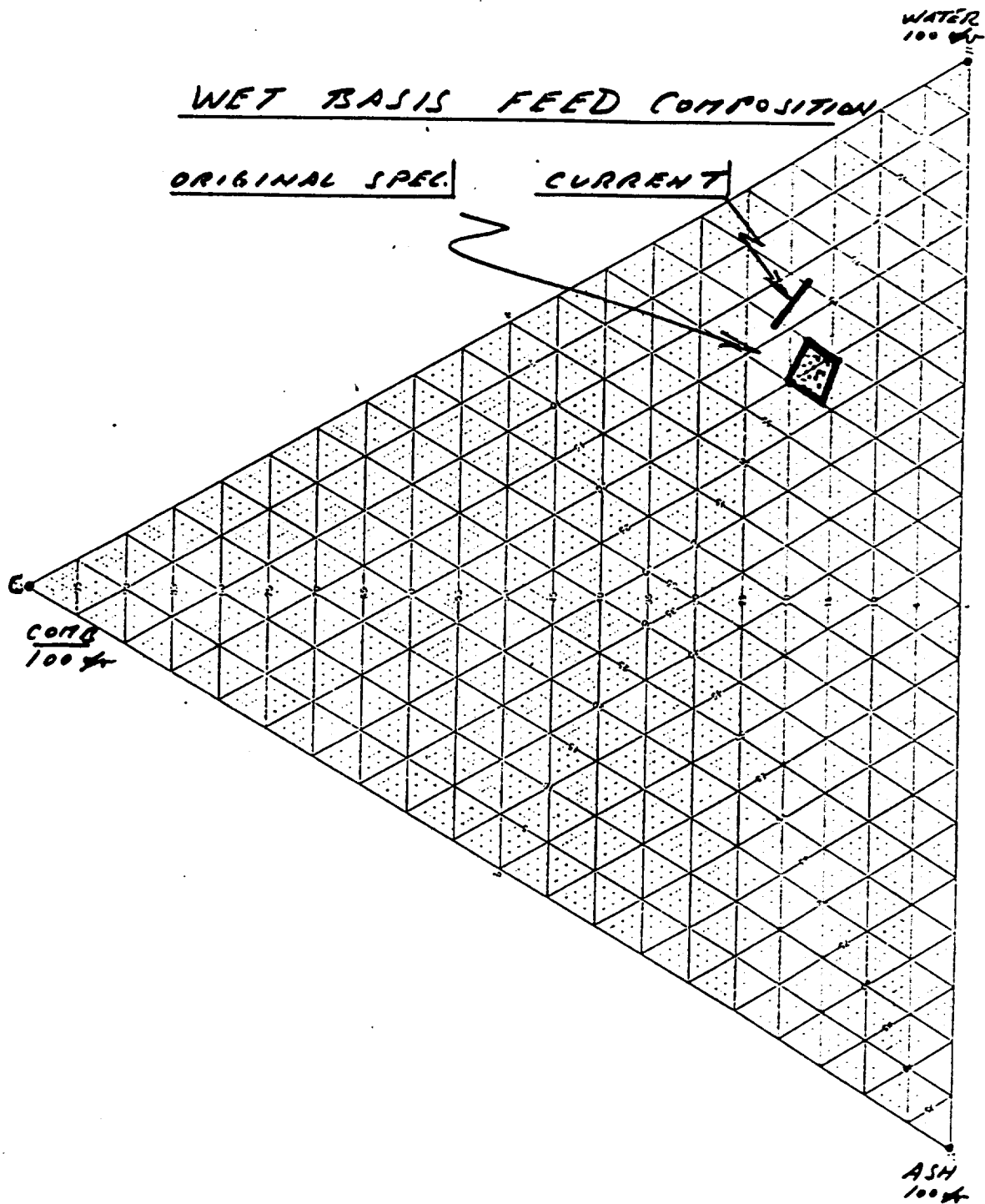
WET FEED RATE POUNDS PER HOUR

5000
9
8
7
6
4500
4
3
2
1
4000
9
8
7
6
3500
4
3
2
1
3000
9
8
7
6
2500

FEED CALIBRATION CURVE
JANUARY 1983



PANEL METER READING



REVISED FEED TARGET
CORRESPONDING TO CURRENT OPERATION

