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SOURCE TEST REPORT

SOURCE EMISSION TESTING OF THE INCINERATOR #2 EXHAUST STACK

AT THE

**CENTRAL CONTRA COSTA SANITARY DISTRICT (CCCSO)
MUNICIPAL WASTEWATER TREATMENT PLANT
MARTINEZ, CALIFORNIA**

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CENTRAL CONTRA COSTA SANITARY DISTRICT
MUNICIPAL WASTEWATER TREATMENT PLANT
MARTINEZ, CALIFORNIA

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PREPARED BY:


MARK LUDWICZAK
ENVIRONMENTAL ENGINEER

APPROVED BY:


DAVID GALSON, P.E.
DEPARTMENT MANAGER

GALSON TECHNICAL SERVICES
2116 BERKELEY WAY
BERKELEY, CA 94704
PHONE # (415) 848-0389
TELEFAX # (415) 848-0838

ABSTRACT

This report summarizes the results of the source emission testing performed on the sewage sludge incinerator #2 exhaust stack at the Central Contra Costa Sanitary District facility in Martinez, California. Testing was conducted by Galson Technical Services, Inc. during the period from April 10 to 13, 1990 to determine emissions of hydrochloric acid, formaldehyde, benzene, vinyl chloride, particulate matter, twelve metals (including hexavalent chromium), polychlorinated dibenzo-p-dioxins and dibenzofurans (PCDD/PCDF), and polycyclic aromatic hydrocarbons (PAH). In addition, carbon monoxide (CO) and total hydrocarbon (THC) levels were continuously monitored throughout the testing. The primary purpose of the test program was to develop emission data, as required by the Bay Area Air Quality Management District (BAAQMD); in particular, as related to the California Air Toxics "Hot Spots" Information and Assessment Act of 1987 (AB 2588). The CO and THC data were collected for in-house purposes.

Results of the test program are summarized below:

Parameter	Concentration	Mass Emission Rate	Emission Ratio
HCl	0.54 mg/dscm	18.0 gm/hr	10.8 gm/ton
Formaldehyde	50 ppb	2.1 gm/hr	1.2 gm/ton
Benzene	4.7 ppb	0.5 gm/hr	0.3 gm/ton
Vinyl Chloride	< 3 ppb	< 0.3 gm/hr	< 0.2 gm/ton
Particulate	0.004 gr/dscf	0.67 lbs/hr	0.42 lbs/ton
Metals:			
Arsenic	< 0.004 mg/dscm	0.14 gms/hr	0.09 gm/ton
Beryllium	< 0.001 mg/dscm	< 0.02 gms/hr	< 0.01 gm/ton
Cadmium	0.010 mg/dscm	0.33 gms/hr	0.21 gm/ton
Chromium			
- total	0.011 mg/dscm	0.37 gms/hr	0.24 gm/ton
- hexavalent	< 0.003 mg/dscm	< 0.1 gm/hr	< 0.06 gm/ton
Copper	0.045 mg/dscm	1.5 gms/hr	0.94 gm/ton
Lead	0.024 mg/dscm	0.8 gms/hr	0.50 gm/ton
Manganese	0.138 mg/dscm	4.5 gms/hr	2.7 gm/ton
Mercury	0.070 mg/dscm	2.3 gms/hr	1.5 gm/ton
Nickel	0.002 mg/dscm	0.06 gms/hr	0.04 gm/ton
Selenium	0.012 mg/dscm	0.39 gms/hr	0.24 gm/ton
Zinc	1.59 mg/dscm	53 gms/hr	35 gm/ton

Parameter	Concentration	Mass Emission Rate	Emission Ratio
<u>PCDD/PCDF</u>			
Total TCDD	< 0.03 ng/dscm	< 1.0 µg/hr	< 0.7 µg/ton
Total PeCDD	< 0.03 ng/dscm	< 1.0 µg/hr	< 0.7 µg/ton
Total HxCDD	< 0.03 ng/dscm	< 0.8 µg/hr	< 0.5 µg/ton
Total HpCDD	< 0.04 ng/dscm	< 1.2 µg/hr	< 0.8 µg/ton
<u>Total OCDD</u>	<u>< 0.05 ng/dscm</u>	<u>< 1.6 µg/hr</u>	<u>< 1.1 µg/ton</u>
Total PCDD	< 0.17 ng/dscm	< 5.7 µg/hr	< 3.8 µg/ton
Total TCDF	< 0.02 ng/dscm	< 0.7 µg/hr	< 0.4 µg/ton
Total PeCDF	< 0.03 ng/dscm	< 0.9 µg/hr	< 0.6 µg/ton
Total HxCDF	< 0.01 ng/dscm	< 0.5 µg/hr	< 0.3 µg/ton
Total HpCDF	< 0.03 ng/dscm	< 0.9 µg/hr	< 0.6 µg/ton
<u>Total OCDF</u>	<u>< 0.03 ng/dscm</u>	<u>< 1.1 µg/hr</u>	<u>< 0.7 µg/ton</u>
Total PCDF	< 0.12 ng/dscm	< 4.1 µg/hr	< 2.7 µg/ton
<u>PAH Compounds</u>			
Naphthalene ¹	0.17 ng/dscm	552 µg/hr	327 µg/ton
Others	<0.01-0.02ng/dscm	<0.4-0.6 µg/hr	<0.3-0.4 µg/ton
CO	50 ppm	4.3 lbs/hr	2.7 lb/ton
THC (as methane)	12 ppm	0.6 lbs/hr	0.4 lb/ton

Note: Emission Ratio data are presented on a per ton of sludge (dry) basis.

¹ Background contamination suspected; refer to discussion in text.

PROJECT PERSONNEL

Central Contra Costa Sanitary District

William BrennanPlant Operations Manager

Galson Technical Services, Inc.

Chuck Siu, CIH.....Office Manager

Glenn Cass, PE.....Mechanical Engineer

Mark LudwiczakProject Manager

Dale Roberts.....Environmental Engineer

Claire Tanglao.....Environmental Engineer

Kathy PakEnvironmental Technician

Ed Stuber.....Laboratory Coordinator

Zenon Environmental Inc.

John CoburnPresident

Rod Thomson.....Project Manager

Henri Huneault.....Head, GC/MS Services

Alpha Chemical and Biomedical Laboratory

Joe Hodgkins, Ph.D., C.T.....Laboratory Director

Mark Fesler.....Analyst

Air Toxics Ltd

Linda Freeman.....Laboratory Director

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1.0 INTRODUCTION

This report summarizes the results of the source emission testing performed on the sewage sludge Incinerator #2 exhaust stack at the Central Contra Costa Sanitary District facility in Martinez, California. Testing was conducted by Galsón Technical Services, Inc. during the period from April 10 to 13, 1990 to determine emissions of hydrochloric acid, formaldehyde, benzene, vinyl chloride, particulate matter, twelve metals (including hexavalent chromium), polychlorinated dibenzo-p-dioxins and dibenzofurans (PCDD/PCDF), and polycyclic aromatic hydrocarbons (PAH). In addition, carbon monoxide (CO) and total hydrocarbon (THC) levels were continuously monitored throughout the testing. The primary purpose of the test program was to develop emission data, as required by the Bay Area Air Quality Management District (BAAQMD); in particular, as related to the California Air Toxics "Hot Spots" Information and Assessment Act of 1987 (AB 2588). The CO and THC data were collected for in-house purposes.

William Brennan, plant operations manager with CCCSD, was present to coordinate testing activities with the boiler operations and observe test procedures. No representatives of either the BAAQMD or the California Air Resources Board (CARB) were present to observe the testing.

2.0 SOURCE DESCRIPTION

The CCCSD's municipal wastewater treatment plant in Martinez, California is an activated sludge facility with a rated capacity of 45 million gallons per day (MGD). Wastewater flow through the plant averages approximately 38 MGD (dry weather flow), consisting of approximately 98 percent domestic and two percent industrial or commercial wastewater. The plant serves 350,000 people in Central Contra Costa County (California).

Primary and secondary sludge from the treatment plant are combined and gravity thickened, prior to dewatering; lime and a polymer material are added to the sludge during the thickening process to enhance its settling characteristics. The thickened sludge is dewatered by centrifuges to approximately 20-25 percent dry solids. Typically, 185 tons per day (wet basis) of sludge are generated.

The plant is equipped with two Envirotech/BSP multiple hearth incinerators, each with a design capacity of 10 tons/hr (wet basis). Only one of the incinerators is on-line at a given time, operating on a continual basis (24 hours/day). The incinerators contain 11 hearths each, with the top hearth serving as an afterburner. Ten of the hearths are equipped with burners (four per hearth), which can fire natural gas and/or landfill gas; fuel oil is utilized as a back-up fuel. The ash is disposed of in a landfill. Cooling air is provided to the rotating, center shaft of the incinerator to protect the shaft from heat-induced failure. The cooling air passes through the center of the shaft and is either discharged to atmosphere through the stack, or partially recycled to the Hearth #9 chamber as pre-heated combustion air. Use of the shaft cooling air for combustion air is modulated with a damper.

Exhaust gases from the incinerator are passed through an Envirotech multiple cyclone dry scrubber; collected ash is returned to the incinerator for further burning and/or discharge. After exiting the scrubber, the exhaust gases are passed through a Zurn waste heat boiler which produces steam for in-house use. Boiler exhaust gases are then passed through a wet scrubber manufactured by Krebs Engineers. The scrubber contains a venturi quench section followed by a spray baffle chamber. It utilizes a total of approximately 900 gallons per minute of treatment plant effluent (non-chlorinated) as the scrubbing medium, the majority of which is passed through both sections of the scrubber prior to disposal.

Scrubber exhaust gases then pass through an induced draft fan and are discharged to the atmosphere through the exhaust stack at a height of approximately 10 feet above the roof line. Schematic diagrams of the incinerator, the exhaust gas treatment system, and the wet scrubber water supply/disposal system are presented in Appendix I.

3.0 TEST PROGRAM/OPERATING CONDITIONS

Source emission testing was conducted on the Incinerator #2 exhaust stack during the period from April 10 to 13, 1990. Testing was performed to determine emissions of the following pollutants:

- Hydrochloric Acid
- Formaldehyde
- Benzene
- Vinyl Chloride
- Particulate Matter
- Metals (12)
- PCDD/PCDF Compounds (15)
- PAH Compounds (16)
- Carbon Monoxide (CO)
- Total Hydrocarbons (THC)

Testing for each parameter was performed in triplicate, with the exception of the PCDD/PCDF/PAH compounds, for which four tests were conducted, and the CO and THC levels, which were monitored continuously during all tests. Specific test intervals are summarized in the test schedule presented in Table 1.

Testing was generally performed during normal incinerator operating conditions. Sludge feed rates typically averaged between 1.5 and 1.7 tons per hour (tph, dry basis) during the tests; the sludge contained between 21 and 25 percent solids. Landfill gas was utilized as the auxiliary fuel.

Unstable incinerator operations were observed during Test 8; in particular, variations in the moisture content of the sludge caused temperatures in the upper hearths of the incinerator to fluctuate considerably. An additional test (Test 10) was therefore performed on the following day during more stable operating conditions.

Incinerator operating data, including hearth temperatures, furnace draft, shaft rotation rate, and scrubber pressure drop were logged by plant personnel during the testing. In addition, stack gas opacity and furnace oxygen content were continuously monitored and recorded throughout the tests. Sludge feed rate and moisture content data were generally logged at two-hour intervals during the tests. These data are presented in Appendix I.

4.0 TEST METHODS

Testing was performed in accordance with Environmental Protection Agency (EPA) and California Air Resources Board (CARB) methods. The sampling and analytical techniques are described briefly below.

4.1 HCl Testing

HCl emission testing was performed in accordance with CARB Method 421. Sampling was performed isokinetically using 24-point traverses, per CARB Method 1 requirements. A one-hour sampling interval (per test run) was utilized to collect the samples. Once collected, the samples were analyzed for HCl using ion chromatography/conductivity detection.

4.2 Formaldehyde, Benzene, and Vinyl Chloride Testing

Formaldehyde emission testing was conducted in accordance with CARB Method 430. Sampling was performed at a single point near the center of the exhaust stack. Sampling was performed at a constant rate of approximately 0.5 liter per minute (lpm) using a high vacuum diaphragm pump/critical orifice assembly. Test durations of 60 minutes were employed. Collected samples were analyzed using high performance liquid chromatography; all samples were analyzed within seven days of collection.

Benzene and vinyl chloride emission testing was conducted in accordance with CARB Method 410A. Sampling was performed at a single point near the center of the exhaust stack. Exhaust gas samples were collected in a tedar bag; sampling was performed continuously throughout a 50-minute (approximately) test duration at a sampling rate of approximately 0.1 lpm. Collected samples were analyzed for benzene and vinyl chloride using GC/MS; all samples were analyzed within 48 hours of collection.

The formaldehyde and benzene sampling was performed concurrently with the HCl sampling; supporting data collected during these tests (i.e., stack gas flow rate, molecular weight) were utilized to determine the formaldehyde and benzene emission rates (gm/hr).

4.3 Particulate/Metals Testing

Particulate and metals emission testing was performed in accordance with the EPA Draft Multiple Metals Method (dated August 28, 1989). Sampling was performed isokinetically using 24-point traverses, per CARB Method 1 requirements. A two-hour sampling interval (per test run) was utilized to collect the samples. Once collected, the front-half fraction (i.e., filter and probe rinse) of the samples was analyzed gravimetrically to determine total particulate emissions. The samples were then analyzed for the 11 metals listed below using inductively coupled plasma (ICP) or atomic absorption (AA) spectroscopy. Front- and back-half fractions were analyzed separately.

Arsenic	Beryllium
Cadmium	Chromium (Total)
Copper	Lead
Manganese	Mercury
Nickel	Selenium
Zinc	

Hexavalent chromium testing was performed in accordance with CARB Method 425 (draft; July 10, 1989). Sampling was performed isokinetically using 24-point traverses, per CARB Method 1 requirements. A two-hour sampling interval (per test run) was utilized to collect the samples. Once collected, the samples were analyzed for hexavalent chromium colorimetrically. The front- and back-half fractions were combined prior to analysis. The samples were analyzed within 48 hours of collection.

4.4 PCDD/PCDF and PAH Testing

PCDD/PCDF and PAH emission testing was performed in accordance with CARB Methods 428 and 429. Sampling was performed utilizing a Modified Method 5 sampling train, with XAD-2 resin employed as the sorbent. Front-half (probe rinse and filter) and back-half (condenser rinse and resin trap) samples were combined and analyzed utilizing high resolution gas chromatography/mass spectrometry (HRGC/MS). Quantification was provided for the following compounds:

PCDD/PCDF:

2,3,7,8 TCDD
1,2,3,7,8 PeCDD
1,2,3,4,7,8 HxCDD
1,2,3,6,7,8 HxCDD
1,2,3,7,8,9 HxCDD
1,2,3,4,6,7,8 HpCDD
Total TCDD, TCDF
Total PeCDD, PCDF
Total HxCDD, PCDF
Total HpCDD, PCDF
Total OCDD, PCDF

2,3,7,8 TCDF
1,2,3,7,8 PeCDF
2,3,4,7,8 PeCDF
1,2,3,4,7,8 HxCDF
1,2,3,6,7,8 HxCDF
2,3,4,6,7,8 HxCDF
1,2,3,7,8,9 HxCDF
1,2,3,4,6,7,8 HpCDF
1,2,3,4,7,8,9 HpCDF

PAH Compounds:

Naphthalene	Acenaphthylene
Acenaphthene	Fluorene
Phenanthrene	Anthracene
Fluoranthene	Benzo(a)anthracene
Chrysene	Benzo(b)fluoranthene
Benzo(k)fluoranthene	Benzo(a)pyrene
Pyrene	Indeno(1,2,3-cd)pyrene
Dibenz(a,h)anthracene	Benzo(g,h,i)perylene

4.5 CO and THC Monitoring

CO and THC concentrations were monitored in accordance with California Air Resources Board (CARB) Method 100 using the following instrumentation:

CO	Thermo Electron Company (TECO) CO analyzer (Model 48)
THC	Ratfish Instruments THC analyzer (Model RS-55)

Sampling was performed at a single point near the duct centroid. A condenser and glass wool filter were incorporated into the CO sampling train for conditioning of the sample gas (i.e., particulate and moisture removal). A heated sampling line was utilized in conjunction with the THC analyzer to prevent condensation of the gas stream upstream of the analyzer. THC concentrations were measured on a wet basis and corrected to dry conditions using the moisture content of the stack gas; THC levels were quantified as methane.

4.6 General

Integrated stack gas samples were collected and analyzed for %CO₂ and %O₂ utilizing an Orsat apparatus (CARB Method 3). These data were used to determine stack gas molecular weight.

Sampling ports were located in the 41 inch diameter stack at a point 16 feet (4.7 diameters) downstream of a bend in the duct and 5 feet (1.5 diameters) upstream of the stack discharge. The stack was equipped with two test ports which were suitable for isokinetic sampling (i.e., HCl, particulate/metals, PCDD/PCDF/PAH); the ports were positioned 90 degrees apart. A third port, used to collect the formaldehyde and benzene/vinyl chloride samples, was located approximately four feet upstream of the ports used for isokinetic sampling; this port was also used for the CO and THC monitoring.

A preliminary velocity/cyclonic flow traverse of the exhaust stack was conducted in accordance with CARB Methods 1 and 2, prior to the start of testing. These measurements,

as presented in Appendix II, confirmed the acceptability of the test sites (i.e., cyclonic flow was not present). Sketches of the stack configuration and traverse point locations are presented in Appendix II. A more detailed discussion of the test methods is presented in Appendix III.

4.7 Test Equipment Calibration

All test equipment was calibrated either prior to or during use in the field. The CO and THC monitors were calibrated with cylinder gases of known concentration immediately before and after each test period. The dry gas meter/orifice modules were calibrated immediately prior to and following the test program. Pitot tubes were also calibrated prior to use in the field and were visually inspected for damage during the test program. All thermometers, thermocouples, and temperature read-outs are routinely calibrated at six-month intervals, or immediately following any damage/repair. A post-test QA check of the thermocouples was also performed. Calibration data are presented in Appendix IV.

5.0 RESULTS AND DISCUSSION

Test results are summarized in Tables 2 through 8 and are discussed below. Supporting field data and calculations are presented in Appendix V, while laboratory data are summarized in Appendix VI.

5.1 HCl Emission Data (Table 2)

HCl emissions, as presented in Table 2, ranged from 15.5 to 20.3 gm/hr and averaged 18.0 gm/hr. Normalized to sludge feed rate, emissions averaged 10.8 gm/ton (dry).

5.2 Formaldehyde, Benzene, and Vinyl Chloride Emission Data (Table 3)

Referring to Table 3, formaldehyde emissions ranged from 0.9 to 3.2 gm/hr, averaging 2.1 gm/hr. Normalized to sludge feed rate, emissions averaged 1.2 gm/ton (dry). Benzene emissions averaged 0.5 gm/hr during Tests 2 and 3 and were less than 0.4 gm/hr during Test 1. Normalized to sludge feed rate, emissions averaged 0.3 gm/ton, dry (Tests 2 and 3). Vinyl chloride emissions were below the detection limit (0.3 gm/hr, or 0.2 gm/ton (dry)) during all three tests.

5.3 Particulate and Metals Emission Data (Tables 4 and 5)

As presented in Table 4, particulate emissions from the exhaust stack were relatively consistent from test to test, ranging from 0.63 to 0.69 lbs/hr and averaging 0.67 lbs/hr. Normalized to sludge feed rate, emissions averaged 0.42 lbs/ton (dry), or approximately 32 percent of the BAAQMD permissible rate (1.3 lbs/ton).

Referring to Table 5, emissions of the majority of metals averaged less than 1 gm/hr; exceptions included copper (1.5 gm/hr), manganese (4.5 gm/hr), mercury (2.3 gm/hr), and zinc (53 gms/hr) emissions. Beryllium and hexavalent chromium emissions were below detection limits during all three tests.

As expected, the metals were collected predominantly in the front-half of the sampling train (i.e., on the filter or in the probe); chromium, zinc, manganese, and mercury were determined to be present in the back-half of the sampling train as well.

The blank sample contained some of the metals of interest (i.e., arsenic, chromium, manganese, selenium, and zinc). Blank quantities of arsenic, zinc, manganese, and selenium

were low with respect to sample quantities (i.e., less than 20 percent); the blank quantity of chromium averaged approximately 30 percent of sample quantities. The source of the blank-contained metals is not known, although it is believed to be attributable to background sources (e.g., the filter, reagents, solvents) and/or contamination. The data presented in Table 3 are not corrected for the blank-contained quantities.

As was noted in the particulate emission data, emissions of the metals were generally consistent from test to test. Manganese emissions were the most variable, ranging from less than 1 gm/hr (Test 6) to approximately 10 gm/hr (Test 4). The majority of the manganese was determined to be present in the back-half of the sampling train (i.e., Container D), particularly for the Test 1 sample. Considering that manganese is utilized in the back-half of the sampling train to collect mercury¹, it is possible that the source of the back-half manganese may be the impinger solution. Manganese was not determined to be present in the back-half fraction of the field blank.

Test 6 zinc emissions were approximately five times the Test 4 and 5 emissions. Review of the laboratory data (refer to Appendix VI) reveals that the majority of the zinc found in the Test 6 samples was in the Container B sample (the nitric acid rinse of the front-half of the sampling train); in contrast, the zinc quantity in the Test 6 Container A sample was not significantly higher than Tests 4 and 5. The Test 6 zinc emissions are therefore considered biased upward; contamination of the Test 6 B sample is suspected.

5.4 PCDD/PCDF and PAH Emission Data (Tables 6 and 7)

As presented in Tables 6A and 6B, emissions of all of the PCDD and PCDF compounds of interest were below detection limits during all four tests. Detection limits ranged from 0.3 (HxCDF) to 1.9 µg/hr (OCDD); normalized to sludge feed rate, the detection limits ranged from 0.2 to 1.2 µg/ton (dry). Total PCDD emissions averaged less than 5.7 µg/hr (3.8 µg/ton, dry), while total PCDF emissions averaged less than 4.1 µg/hr (2.7 µg/ton, dry). Blank quantities were also below detection limits for all compounds.

¹ As per method specifications, 100 milliliters of potassium permanganate (KMnO₄) in a sulfuric acid solution is placed in the fourth impinger of the sampling train (refer to Appendix III).

Similarly, emissions of all of the PAH compounds were below the detection limit (0.4 to 0.6 mg/hr, or 0.3 to 0.4 mg/ton) during all four test runs, with the exception of naphthalene (refer to Table 7). Relatively high levels of naphthalene were determined to be present in all four samples as well as the field blank¹. The naphthalene data should therefore be considered suspect. Background quantities have been observed in similar blank samples previously submitted for analysis and although the source of the naphthalene is not known, it is suspected to be an impurity and/or a by-product of the break-down of the XAD-2 resin².

As previously noted, relatively unstable incinerator operating conditions were noted during Test 8 and therefore, an additional test (#10) was conducted during normal operations. Review of the data presented in Table 6 and 7 reveals that the unstable operating conditions did not impact observed emissions.

5.5 THC and CO Emission Data (Table 8)

As presented in Table 8, THC concentrations ranged from 9 to 17 ppm (as methane), averaging 12 ppm; corresponding THC emission rates averaged 0.6 lbs/hr (0.4 lbs/ton, dry). These data agree with published emission factors for these types of sources³. CO levels were more variable, ranging from 25 to 74 ppm and averaging 50 ppm; corresponding CO emission rates averaged 4.3 lbs/hr (2.7 lbs/ton, dry).

The data do not indicate that a correlation exists between the levels of THC and/or CO levels observed in the exhaust gas and emissions of the air toxics of interest (i.e., PCDD/PCDF, PAH, formaldehyde, benzene, vinyl chloride).

¹ The field blank sample contained 810 µg of naphthalene, while the quantities determined to be present in the Tests 1 through 4 samples ranged from 26 to 100 µg per sample (refer to the laboratory data presented in Appendix VI).

² XAD is 1,4-divinyl benzene; 1,2-divinyl benzene (an impurity) can react to form naphthalene.

³ 1 lb/ton (AP-42).

5.6 General

Other than noted, no sampling problems were encountered during the test program. Isokinetic sampling conditions were maintained during the HCl, metals, hexavalent chromium, and PCDD/PCDF/PAH tests, with isokinetic percentages within the allowable $100 \pm 10\%$ during all tests (refer to Appendix V). Calibrations of the monitors performed before and after each test period were in agreement (within 2 percent).

Table 1: Summary of the Test Schedule

Test ID - Date	Test Times	Parameters	Sludge Feed Rate (tph ¹)
1 - 4/10/90	1138-1245 1138-1238 1139-1229	HCl, CO, THC Formaldehyde Benzene, Vinyl Chloride	1.7
2 - 4/10/90	1357-1505 1357-1457 1357-1447	HCl, CO, THC Formaldehyde Benzene, Vinyl Chloride	1.6
3 - 4/10/90	1554-1702 1554-1654	HCl, CO, THC Formaldehyde	1.7
3B - 4/10/90	1653-1730	Benzene, Vinyl Chloride	1.7
4 - 4/11/90	1027-1240	Particulate, Metals (11) Hex. Chromium, CO, THC	1.7
5 - 4/11/90	1410-1621	Particulate, Metals (11) Hex. Chromium, CO, THC	1.6
6 - 4/12/90	0833-1050	Particulate, Metals(11) Hex. Chromium, CO, THC	1.5
7 - 4/12/90	1219-1546	PCDD/PCDF, PAH, CO, THC	1.5
8 - 4/12/90	1645-2005	PCDD/PCDF, PAH, CO, THC	1.5
9 - 4/13/90	1010-1340	PCDD/PCDF, PAH, CO, THC	1.5
10 - 4/13/90	1455-1823	PCDD/PCDF, PAH, CO, THC	1.5

¹ Dry basis.

Table 2: Summary of Results - HCl Emissions

Test # (Date; Times)	Sludge Feed Rate (tph) ¹	HCl Emissions		
		(mg/dscm)	(gm/hr)	(gm/ton)
1 (4/10/90; 1138-1245)	1.7	0.47	15.5	9.1
2 (4/10/90; 1357-1505)	1.6	0.55	18.3	11.4
3 (4/10/90; 1554-1702)	1.7	0.60	20.3	12.0
Average	1.7	0.54	18.0	10.8

¹ Dry basis.

Table 3: Summary of Results - Formaldehyde, Benzene, and Vinyl Chloride Emissions

Test # (Date; Times)	Sludge Feed Rate (tph) ¹	Parameter	Emissions		
			(ppb)	(gm/hr)	(gm/ton)
1 (4/10/90; 1138-1238)	1.7	Formaldehyde	80	3.2	1.9
		Benzene	< 4	< 0.4	< 0.2
		Vinyl Chloride	< 4	< 0.3	< 0.2
2 (4/10/90; 1357-1457)	1.6	Formaldehyde	21	0.9	0.6
		Benzene	5.5	0.6	0.4
		Vinyl Chloride	< 4	< 0.3	< 0.2
3 (4/10/90; 1554-1654; 1653-1730) ²	1.7	Formaldehyde	49	2.1	1.2
		Benzene	3.8	0.4	0.3
		Vinyl Chloride	< 2	< 0.2	< 0.1
Average	1.7	Formaldehyde	50	2.1	1.2
		Benzene ³	4.7	0.5	0.3
		Vinyl Chloride	< 3	< 0.3	< 0.2

¹ Dry Basis

² Formaldehyde sampling was performed from 1554-1654, while the benzene and vinyl chloride sample was collected from 1653-1730.

³ Average values do not include Test 1 emissions, which were below the detection limit.

Table 4: Summary of Results - Particulate Emissions

Test # (Date; Times)	Sludge Feed Rate (tph) ¹	Particulate Emissions			Percent of Permissible ²
		(gr/dscf)	(lbs/hr)	(lbs/ton)	
4 (4/11/90; 1027-1240)	1.7	0.0043	0.69	0.41	32
5 (4/11/90; 1410-1621)	1.6	0.0041	0.69	0.43	33
6 (4/12/90; 0833-1050)	1.5	0.0037	0.63	0.42	32
Average	1.6	0.0040	0.67	0.42	32

¹ Dry basis.

² 1.30 lbs/ton(dry); BAAQMD Reg. 10, Rule 13.

Table 5: Summary of Results - Metals Emissions

Metal	Test 4		Test 5		Test 6		Average	
	mg/dscm	gms/hr gm/ton ¹	mg/dscm	gms/hr gm/ton ¹	mg/dscm	gms/hr gm/ton ¹	mg/dscm	gm/hr gm/ton ¹
Arsenic	0.006	0.18 0.10	0.003	0.11 0.07	0.004	0.15 0.10	0.004	0.14 0.09
Beryllium	<0.001	<0.02 <0.01	<0.001	<0.02 <0.01	<0.001	<0.02 <0.02	<0.001	<0.02 <0.01
Cadmium	0.008	0.25 0.15	0.010	0.34 0.22	0.012	0.39 0.26	0.010	0.33 0.21
Chromium: • Total • Hexavalent ²	0.010 <0.003	0.31 <0.10 0.18 <0.05	0.009 <0.003	0.31 <0.10 0.19 <0.06	0.015 <0.003	0.50 <0.10 0.34 <0.06	0.011 <0.003	0.37 <0.10 0.24 <0.06
Copper	0.037	1.19 0.70	0.043	1.42 0.89	0.054	1.84 1.23	0.045	1.49 0.94
Lead	0.018	0.57 0.34	0.026	0.88 0.55	0.027	0.91 0.61	0.024	0.79 0.50
Manganese	0.310 ³	9.95 ³ 5.85 ³	0.080	2.66 1.68	0.023	0.76 0.51	0.138	4.46 2.67
Mercury	0.043	1.39 0.82	0.064	2.12 1.32	0.104	3.51 2.34	0.070	2.34 1.49
Nickel	0.002	0.07 0.04	0.001	0.05 0.03	<0.004	<0.12 <0.08	0.002 ⁴	0.06 ⁴ 0.04 ⁴
Selenium	0.010	0.31 0.18	0.012	0.40 0.25	0.013	0.44 0.29	0.012	0.39 0.24
Zinc	0.648	20.8 12.2	0.716	23.7 14.8	3.40 ³	115 ³ 76.6 ³	1.59	53.2 34.6

1 Dry Basis.

2 Hexavalent chromium emissions were determined using a separate sampling train; testing was performed concurrently with the other metals.

3 Data suspect; refer to discussion in text.

4 Average of Tests 4 and 5 data; Test 6 emissions were below the detection limit.

Table 6A: Summary of Results - PCDD Emissions

Test # (Date)	#7 4/12/90			#8 4/12/90			#9 4/13/90			#10 4/13/90			Average		
	(ng/ decim)	(µg/ hr)	(µg/ ton)	(ng/ decim)	(µg/ hr)	(µg/ ton)	(ng/ decim)	(µg/ hr)	(µg/ ton)	(ng/ decim)	(µg/ hr)	(µg/ ton)	(ng/ decim)	(µg/ hr)	(µg/ ton)
2378 TCDD	<0.011	<0.4	<0.2	<0.028	<0.9	<0.6	<0.026	<0.9	<0.6	<0.047	<1.6	<1.0	<0.028	<0.9	<0.6
Total TCDD	<0.011	<0.4	<0.2	<0.028	<0.9	<0.6	<0.034	<1.1	<0.7	<0.054	<1.8	<1.2	<0.032	<1.0	<0.7
12378 PeCDD	<0.029	<1.0	<0.6	<0.024	<0.8	<0.5	<0.022	<0.7	<0.5	<0.028	<0.9	<0.6	<0.028	<0.9	<0.6
Total PeCDD	<0.029	<1.0	<0.6	<0.024	<0.8	<0.5	<0.023	<0.7	<0.5	<0.047	<1.6	<1.0	<0.031	<1.0	<0.7
123478 HxCDD	<0.024	<0.8	<0.5	<0.020	<0.7	<0.4	<0.028	<0.9	<0.6	<0.025	<0.8	<0.6	<0.024	<0.8	<0.5
123678 HxCDD	<0.024	<0.8	<0.5	<0.021	<0.7	<0.5	<0.029	<0.9	<0.6	<0.025	<0.8	<0.6	<0.025	<0.8	<0.5
123789 HxCDD	<0.024	<0.8	<0.5	<0.020	<0.7	<0.4	<0.029	<0.9	<0.6	<0.026	<0.9	<0.6	<0.025	<0.8	<0.5
Total HxCDD	<0.024	<0.8	<0.5	<0.021	<0.7	<0.5	<0.029	<0.9	<0.6	<0.026	<0.9	<0.6	<0.025	<0.8	<0.5
1234678 HpCDD	<0.026	<0.9	<0.6	<0.055	<1.8	<1.2	<0.025	<0.8	<0.6	<0.041	<1.4	<0.9	<0.037	<1.2	<0.8
Total HpCDD	<0.026	<0.9	<0.6	<0.055	<1.8	<1.2	<0.025	<0.8	<0.6	<0.044	<1.5	<1.0	<0.038	<1.3	<0.9
12346789 OCDD	<0.053	<1.8	<1.2	<0.046	<1.5	<1.0	<0.040	<1.3	<0.9	<0.056	<1.9	<1.2	<0.049	<1.6	<1.1
Total OCDD	<0.053	<1.8	<1.2	<0.046	<1.5	<1.0	<0.040	<1.3	<0.9	<0.056	<1.9	<1.2	<0.049	<1.6	<1.1
TOTAL PCDD	<0.14	<4.8	<3.2	<0.18	<5.8	<3.8	<0.15	<4.9	<3.3	<0.23	<7.5	<5.0	<0.17	<5.7	<3.8

Table 6B: Summary of Results - PCDF Emissions

Test # (Date)	#7 4/12/90			#8 4/12/90			#9 4/13/90			#10 4/13/90			Average		
	(ng/ decim)	(µg/ hr)	(µg/ ton)	(ng/ decim)	(µg/ hr)	(µg/ ton)	(ng/ decim)	(µg/ hr)	(µg/ ton)	(ng/ decim)	(µg/ hr)	(µg/ ton)	(ng/ decim)	(µg/ hr)	(µg/ ton)
2378 TCDF	<0.008	<0.3	<0.2	<0.012	<0.4	<0.3	<0.012	<0.4	<0.3	<0.038	<1.2	<0.8	<0.017	<0.6	<0.4
Total TCDF	<0.008	<0.3	<0.2	<0.013	<0.4	<0.3	<0.012	<0.4	<0.3	<0.049	<1.6	<1.1	<0.020	<0.7	<0.4
12378 PeCDF	<0.021	<0.7	<0.5	<0.018	<0.6	<0.4	<0.025	<0.8	<0.5	<0.028	<0.9	<0.6	<0.023	<0.7	<0.5
23478 PECDF	<0.022	<0.7	<0.5	<0.019	<0.6	<0.4	<0.025	<0.8	<0.5	<0.028	<0.9	<0.6	<0.023	<0.8	<0.5
Total PeCDF	<0.022	<0.7	<0.5	<0.019	<0.6	<0.4	<0.043	<1.4	<0.9	<0.029	<1.0	<0.7	<0.028	<0.9	<0.6
123478 HxCDF	<0.013	<0.4	<0.3	<0.013	<0.4	<0.3	<0.012	<0.4	<0.3	<0.018	<0.6	<0.4	<0.014	<0.5	<0.3
123678 HxCDF	<0.013	<0.4	<0.3	<0.014	<0.5	<0.3	<0.012	<0.4	<0.3	<0.018	<0.6	<0.4	<0.014	<0.5	<0.3
234678 HxCDF	<0.013	<0.4	<0.3	<0.014	<0.5	<0.3	<0.012	<0.4	<0.3	<0.017	<0.6	<0.4	<0.014	<0.5	<0.3
123789 HxCDF	<0.013	<0.4	<0.3	<0.013	<0.4	<0.3	<0.012	<0.4	<0.3	<0.017	<0.6	<0.4	<0.014	<0.5	<0.3
Total HxCDF	<0.013	<0.4	<0.3	<0.014	<0.5	<0.3	<0.013	<0.4	<0.3	<0.018	<0.6	<0.4	<0.014	<0.5	<0.3
1234678 HPCDF	<0.017	<0.6	<0.4	<0.022	<0.7	<0.5	<0.017	<0.6	<0.4	<0.050	<1.7	<1.1	<0.027	<0.9	<0.6
1234789 HPCDF	<0.017	<0.6	<0.4	<0.023	<0.8	<0.5	<0.017	<0.6	<0.4	<0.053	<1.7	<1.2	<0.027	<0.9	<0.6
Total HPCDF	<0.017	<0.6	<0.4	<0.023	<0.8	<0.5	<0.017	<0.6	<0.4	<0.053	<1.7	<1.2	<0.027	<0.9	<0.6
1234678 OCDF	<0.031	<1.0	<0.7	<0.032	<1.1	<0.7	<0.031	<1.0	<0.7	<0.041	<1.4	<0.9	<0.034	<1.1	<0.7
Total OCDF	<0.031	<1.0	<0.7	<0.032	<1.1	<0.7	<0.031	<1.0	<0.7	<0.041	<1.4	<0.9	<0.034	<1.1	<0.7
TOTAL PCDF	<0.091	<3.0	<2.0	<0.10	<3.3	<2.2	<0.12	<3.8	<2.5	<0.19	<6.3	<4.2	<0.12	<4.1	<2.7

Table 7: Summary of Results - PAH Emissions

Test #	PAH Compound	7 ng/ decim	7 µg/ hr	7 µg/ ton	8 ng/ decim	8 µg/ hr	8 µg/ ton	9 ng/ decim	9 µg/ hr	9 µg/ ton	10 ng/ decim	10 µg/ hr	10 µg/ ton	ng/ decim	AVG µg/ hr	µg/ ton
	Naphthalene	14	464	309	14	455	303	31	1,020	679	8	270	18	17	552	327
	Acenaphthylene	<0.02	<0.6	<0.4	<0.02	<0.6	<0.4	<0.02	<0.6	<0.4	<0.02	<0.6	<0.4	<0.02	<0.6	<0.4
	Acenaphthene	<0.02	<0.6	<0.4	<0.02	<0.6	<0.4	<0.02	<0.6	<0.4	<0.02	<0.6	<0.4	<0.02	<0.6	<0.4
	Fluorene	<0.02	<0.6	<0.4	<0.02	<0.6	<0.4	<0.02	<0.6	<0.4	<0.02	<0.6	<0.4	<0.02	<0.6	<0.4
	Phenanthrene	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3
	Anthracene	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3
	Fluoranthene	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3
	Pyrene	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3
	Chrysene	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3
	B(a)A ¹	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3
	B(b)F ¹	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3
	B(k)F ¹	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3
	B(a)P ¹	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3
	I(c,d)P ¹	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3
	D(a,h)A ¹	<0.02	<0.6	<0.4	<0.02	<0.6	<0.4	<0.02	<0.6	<0.4	<0.02	<0.6	<0.4	<0.02	<0.6	<0.4
	B(ghi)P ¹	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3	<0.01	<0.4	<0.3

1 B(a)A Benzo(a)anthracene
 B(b)F Benzo(b)fluoranthene
 B(k)F Benzo(k)fluoranthene
 B(a)P Benzo(a)pyrene
 I(c,d)P Indeno(1,2,3-cd)pyrene
 D(a,h)A Dibenzo(a,h)anthracene
 B(ghi)P Benzo(ghi)perylene

Table 8: Summary of Results - THC and CO Emissions

Test ID (Date; Times)	Sludge Feed Rate (tph) ²	THC ¹			Carbon Monoxide		
		ppm	lbs/hr	lbs/ton ²	ppm	lbs/hr	lbs/ton ²
1 - 4/10/90 (1138-1245)	1.7	13	0.6	0.4	35	2.9	1.7
2 - 4/10/90 (1357-1505)	1.6	9	0.4	0.3	74	6.3	3.9
3 - 4/10/90 (1554-1702)	1.7	10	0.5	0.3	26	2.3	1.3
4 - 4/11/90 (1027-1240)	1.7	11	0.5	0.3	29	2.4	1.4
5 - 4/11/90 (1410-1621)	1.6	10	0.5	0.3	57	4.8	3.0
6 - 4/12/90 (0835-1050)	1.5	13	0.6	0.4	61	5.3	3.5
7 - 4/12/90 (1219-1546)	1.5	14	0.7	0.4	51	4.3	2.9
8 - 4/12/90 (1645-2005)	1.5	11	0.5	0.3	71	6.0	4.0
9 - 4/13/90 (1010-1340)	1.5	16	0.8	0.5	59	4.9	3.3
10 - 4/13/90 (1455-1823)	1.5	17	0.8	0.6	39 ³	3.3	2.2
----- Average	1.6	12	0.6	0.4	50	4.3	2.7

1 As methane.

2 Dry basis.

3 Average level monitored from 1455-1744; CO levels exceeded 200 ppm from 1744-1823.

APPENDIX I: PROCESS OPERATING DATA

TO ATMOSPHERE- Scrubber Outlet (Stack) Test Site

130 PSIG STEAM

BOILER FEED WATER

WASTE HEAT RECOVERY BOILER

BOILER SLOW-BURN

SHAFT COOLING AIR BYPASS

AFTER BURNER ZONE

MEGUSA

FURNACE

DEHYDRATED GRIT SCREW CONVEYOR

CENTRIFUGED SLUDGE FEED

SHAFT COOLING AIR RETURN

DUCT RETURN SCREW CONVEYOR

TO OPAIN

AUXILIARY AIR SUPPLY DUCT

THICKENED SLUDGE FEED

AIR INLET PORT (TYP.)

AUXILIARY SHAFT COOLING AIR FAN

TO ASH DISPOSAL SYSTEM

CENTER SHAFT DRIVE

SHAFT COOLING AIR FAN

COMBUSTION AIR FAN

TO ATMOSPHERE

EMERGENCY BYPASS STACK

MULTI-CYCLON DRY SCRUBBER

FUEL OIL TO BURNER

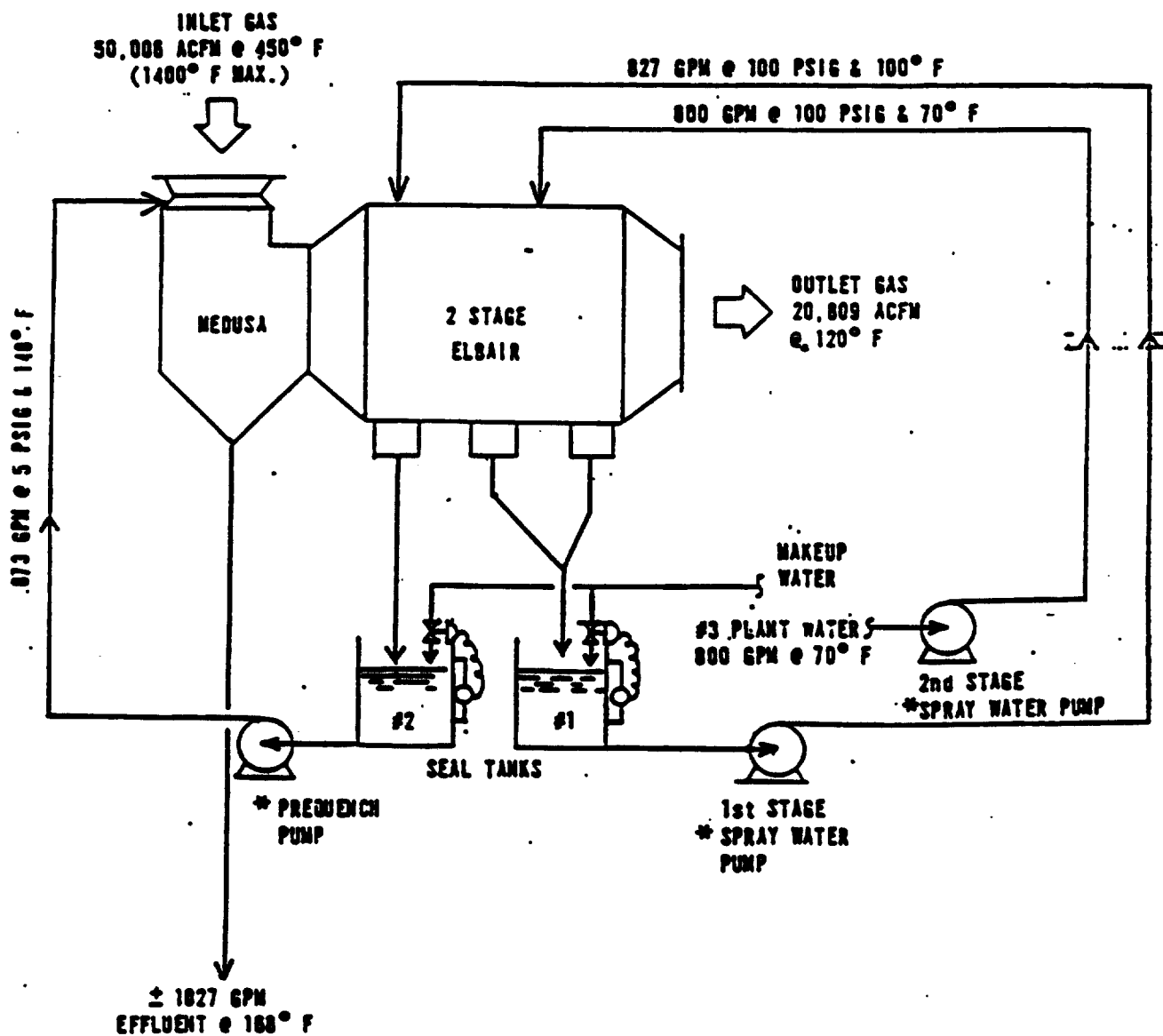
NATURAL GAS TO BURNERS

FUEL OIL TO BURNERS

LANDFILL GAS TO BURNERS

NO LONGER IN USE

**Figure I-2: The Wet Scrubber Water Supply/Disposal System
- Flow Diagram**



**NOTES: ABOVE VALUES DESIGN
FLOW**

*** SECOND PUMP NOT
RUNNING**

Table I-1: Summary of Incinerator Operating Data - Tests 1-6

Test# - Date (Times)	Sludge Data		Avg. Hearth Temperatures (°F)					Scrubber ΔP (In. H ₂ O)	Exhaust Gas Data	
	Feed Rate ¹ (gph)	Solids Content (%)	1	2	3	4	5		O ₂ Content (%)	Opacity (%)
<u>HCl, Benzene, Vinyl Chloride, Formaldehyde Tests:</u>										
1 - 4/10/90 (1138-1245)	1.7 (7.6)	22.5	1249	1243	1540	1567	1372	8.3	5.3	5.0
2 - 4/10/90 (1357-1505)	1.6 (7.7)	21.0	1253	1245	1506	1550	1333	8.4	7.2	5.2
3 - 4/10/90 (1554-1702)	1.7 (7.0)	23.5	1284	1269	1542	1567	1307	--3	5.8	5.6
3B2 - 4/10/90 (1653-1730)	1.7 (7.4)	22.3	1431	1357	1823	1809	1271	--3	8.4	5.2
Average	1.7 (7.4)	22.3	1304	1278	1603	1623	1321	8.4	6.7	5.2
<u>Metals, Hexachloro Chromium Tests:</u>										
4 - 4/11/90 (1027-1243)	1.7 (7.7)	21.4	1284	1273	1531	1584	1216	7.5	5.6	4.6
5 - 4/11/90 (1410-1624)	1.6 (7.6)	21.6	1245	1228	1536	1614	1381	8.3	5.6	5.0
6 - 4/12/90 (0833-1052)	1.5 (6.8)	23.0	1268	1238	1559	1614	1095	7.9	7.4	5.0
Average	1.6 (7.4)	22.0	1266	1246	1542	1604	1231	7.9	6.2	4.9

¹ Dry basis; parenthetical values represent wet feed rates.

² Benzene and vinyl chloride testing (only) was performed during Test 3B; benzene and vinyl chloride testing was not performed during Test 3.

³ No data were recorded.

Table I-2: Summary of Incinerator Operating Data - Tests 7 - 10

Test# - Date (Times)	Sludge Data		Avg. Hearth Temperatures (°F)					Scrubber ΔP (in. H ₂ O)	Exhaust Gas Data	
	Feed Rate ¹ (tph)	Solids Content (%)	1	2	3	4	5		O ₂ Content (%)	Opacity (%)
PCDD/PCDF, PAH Tests:										
7 - 4/12/90 (1219-1546)	1.5 (6.4)	24.0	1239	1194	1510	1552	1058	7.8	8.0	5.4
8 - 4/12/90 (1645-2005)	1.5 (6.3)	24.5	1254	1133	1531	1565	1061	7.8	6.5	5.2
9 - 4/13/90 (1010-1340)	1.5 (6.6)	24.0	1245	1072	1460	1492	1231	7.9	6.5	5.3
10 - 4/13/90 (1455-1823)	1.5 (6.4)	24.1	1197	1088	1509	1509	1193	7.4	6.7	5.5
Average	1.5 (6.4)	24.2	1233	1122	1503	1530	1136	7.7	6.9	5.4

¹ Dry basis; parenthetical values represent wet feed rates.

**Incinerator Operating Data - HCl, Benzene,
Vinyl Chloride, and Formaldehyde Tests
(4/10/90)**

SLUDGE FEED DATA SHEET

DATE 4-10-90

Example Time	Food Concentration	Controls Concentration	Cake Concentration	Capture = $\frac{(\text{food} \cdot \text{controls}) \cdot \text{cake}}{(\text{cake} \cdot \text{controls}) \cdot \text{food}}$	Control Flow gpm	Dry Furnace Feed - Flow = $0.34 \times 80 \times$ feed = capture	Wet Furnace Feed = Dry Feed cake
	8% = .08	4% = 0.004	28% = 0.28	$\frac{(.08 \cdot .004 \cdot .28)}{(.28 \cdot .004 \cdot .08)}$ = 0.06	85 gpm	$85 \times 0.34 \times 80 \times .08 = .86$ = 2424 lb/hr	$\frac{2424}{.28} = 8,657$ lb/hr
#1 2400	.062	.0046	.250	94	76	2,223	8,895 (17,92)
#2 0200	.049	.0063	.235	92	73	2,090	8,896 (17,92)
		.0054	.223	91	74	1,654	7,419 (15,186)
		.0034	.213	94	76	1,654	7,767 (15,186)
0400	.046	.0019	.218	96	76	1,691	7,761 (15,371)
		.0010	.217	98	73	1,651	7,610 (15,371)
0600	.049	.0029	.190	95	77	1,803	9,493 (17,646)
		.0010	.219	98	74	1,785	8,153 (17,646)
0800	.045	.0046	.220	94	76	1,616	7,345
		.0049	.210	91	74	1,520	7,280 14,585
1000	.047	.0031	.220	95	75	1,671	7,596 15,052
		.0052	.210	91	73	1,566	7,456 15,052
1200	.048	.0040	.230	93	76	1,703	7,404 15,187
		.0030	.220	95	75	1,712 (1.71)	7,783 (7.59)
1400	.046	.0057	.220	94	76	1,636	7,437 15,416
		.0057	.200	94	74	1,596 (1.62)	7,779 (7.71)
1600	.050	.0061	.24	88	75	1,647	6,864 13,993
		.0044	.23	91	75	1,711 (1.68)	7,129 (7.00)
1800	.047	.0046	.21	90	75	1,591	7,577 15,722
		.0033	.20	93	75	1,640 (1.62)	8,200 (7.81)
2000	.046	.0045	.21	90	75	1,557	7,414 14,316
		.0037	.23	92	75	1,587	8,902 14,316
2200	.046	.0042	.22	91	75	1,568	7,130 14,363
		.0036	.22	92	75	1,591	7,233 14,363

- Formaldehyde
- HCL
- Benzene

- Formaldehyde
2-HCL
Benzene

Formaldehyde
3-HCL

Benzene

Test 1 1/5

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-10-90 @ 1145

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE %	AIR PORT POSITION	COMMENTS
1	1269	1200	1	0		
2	1271	1210	4	90%		
3	1594	1400	2	0		
4	1610	off 1400	0	0		
5	1471	1400	3	30		
6	1017	1000	3	25		
7	476	off 400	0	0	70%	
8	433	400	0	0		
9	506	400	0	0	70%	
10	453	400	0	0		
11	200	-	-	-		

SHAFT RECYCLE AIR: 0 I.D. FAN % 54% SCRUBBER DP 8.38

PERCENT OXYGEN: 6.4 DRAFT: -.25

SHAFT RPM: 2.2 OPACITY: 5.00%

Phil Hunter

Test 1 $\frac{2}{5}$

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-10-90 @ 1200

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE %	AIR PORT POSITION %	COMMENTS
1	1254	1200	1	0		
2	1257	1210	4	95		
3	1576	1400	2	0		
4	1607	1400	0	0		
5	1390	1400	3	0		
6	948	900	3	25		
7	365	400	0	0	70	
8	294	400	0	0		
9	273	400	0	0	70	
10	261	400	0	0		
11	200		—	—		

SHAFT RECYCLE AIR: 0 I.D. FAN % 53% SCRUBBER DP 8.06PERCENT OXYGEN: 5.7% DRAFT: -.27SHAFT RPM: 2.2 OPACITY: 5.04

Phil Hunter

Test 1 $\frac{3}{5}$

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-10-90 1215

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE %	AIR PORT POSITION %	COMMENTS
1	1236	1200	1	0		
2	1232	1210	4	100		
3	1545	1400	2	0		
4	1582	1400	0	0		
5	1344	1400	2	0		
6	898	900	3	25		
7	354	400	0	0	70	
8	276	400	0	0		
9	256	400	0	0	70	
10	249	400	0	0		
11	200	—	—	—		

SHAFT RECYCLE AIR: 0 I.D. FAN % 54% SCRUBBER DP 8.21

PERCENT OXYGEN: 7.3 DRAFT: -.32

SHAFT RPM: 2.2 OPACITY: 4.80

Phil Hunterman

Test 1 ⁴/₅

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-10-90 1230

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1233	1200	1	Ø		
2	1209	1210	4	100		
3	1474	1400	2	Ø		
4	1527	Ø 1400	Ø	Ø		
5	1323	1400	2	Ø		
6	904	900	3	40		
7	366	Ø 400	Ø	Ø	70	
8	261	400	Ø	Ø		
9	233	400	Ø	Ø	75	
10	230	400	Ø	Ø		
11	200	-	-	-		

SHAFT RECYCLE AIR: Ø I.D. FAN % 527 SCRUBBER DP 8.42PERCENT OXYGEN: 3.8 DRAFT: -1.22SHAFT RPM: 2.2 OPACITY: 5.17

Phil Hunterman

Test 1 5

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-10-90 1245

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE %	AIR PORT POSITION	COMMENTS
1	1252	1200	1	0		
2	1246	1210	4	30		
3	1491	1400	2	0		
4	1511	1400	0	0		
5	1332	1400	2	50		
6	944	900	3	0		
7	541	1400	0	0	70	
8	331	400	0	0		
9	235	400	0	0	75	
10	237	400	0	0		
11	200	—	—	—		

SHAFT RECYCLE AIR: 0 I.D. FAN % 53 SCRUBBER DP 8.38PERCENT OXYGEN: 3.4 DRAFT: -1.28SHAFT RPM: 2.2 OPACITY: 5.19*Phil Hunter*

TEST 2 1/5

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-10-90 1400

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1254	1220	1	0		
2	1252	1220	4	32		
3	1560	1420	2	0		
4	1599	1380	—	0		
5	1334	1330	2	85		
6	895	900	3	15		
7	413	400	—	0	83	
8	258	380	—	0		
9	200	400	—	0	83	
10	206	380	—	0		
11	200					

SHAFT RECYCLE AIR: 0 I.D. FAN % 55.5 SCRUBBER DP 8.52

PERCENT OXYGEN: 6.3 DRAFT: 0.35

SHAFT RPM: 2.2 OPACITY: 5.5

TEST 2 1/5

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 470-80 1445

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1257	1220	1	Q		
2	1242	1220	4	38		
3	1551	1420	2	Q		
4	1592	1380	Q	Q		
5	1335	1220	2	35		
6	897	800	3	15		
7	390	400	Q	Q	80%	
8	242	380	Q	Q		
9	200	400	Q	Q	80%	
10	200	300	Q	Q		
11	200					

SHAFT RECYCLE AIR: Q I.D. FAN % 54% SCRUBBER DP 8.17PERCENT OXYGEN: 6.2 DRAFT: -36SHAFT RPM: 2.2 OPACITY: 5.24

TEST 2 5/5

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-10-90 1500

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1250	1200	1	0		
2	1240	1210	4	50		
3	1409	1400	2	80		
4	1455	1400	0	0		
5	1326	1400	2	0		
6	897	900	3	20		
7	384	400	0	0	70	
8	286	400	0	0		
9	236	400	0	0	70	
10	200	400	0	0		
11	200	-	-	-		

SHAFT RECYCLE AIR: 0 I.D. FAN % 52 SCRUBBER DP 8.33

PERCENT OXYGEN: 8.9 DRAFT: -37

SHAFT RPM: 2.2 OPACITY: 4.84

Phil Hunterman

947-0462

TEST 3 1/5

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 7/10/90 1600

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1252	1250	1	0%		
2	1247	1225	4	30%		
3	1402	1400	2	90%		
4	1408	1400	0	0%		
5	1319	1300	2	0%		
6	910	900	3	0%		
7	460	400	0	0%	50%	
8	256	400	0	0%		
9	200	400	0	0%	60%	
10	200	400	0	0%		
11	200	400	0	0%		

SHAFT RECYCLE AIR: 0 I.D. FAN % 54 SCRUBBER DP PERCENT OXYGEN: 3.4 DRAFT: -1.35SHAFT RPM: 2.2 OPACITY: 7.67

TEST 3 2/5

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4/14/90 1615

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1252	1250	1	09%		
2	1249	1225	4	65%		
3	1504	1400	2	09%		
4	1530	1400	6	09%		
5	1312	1300	2	09%		
6	984	900	3	25%		
7	366	400	6	09%	100%	
8	218	400	6	09%		
9	200	400	6	09%	100%	
10	200	400	6	09%		
11	200	400	6	09%		

SHAFT RECYCLE AIR: 6 I.D. FAN % 56 SCRUBBER DP

PERCENT OXYGEN: 7.2 DRAFT: -0.35

SHAFT RPM: 2.2 OPACITY: 4.87

TEST 3 3/5

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4/10/90 1630

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1260	1250	1	0%		
2	1277	1225	4	40%		
3	1472	1400	2	15%		
4	1527	1400	Ø	0%		
5	1297	1300	2	35%		
6	890	900	3	25%		
7	361	400	Ø	0%	100%	
8	210	400	Ø	0%		
9	200	400	Ø	0%	100%	
10	200	400	Ø	0%		
11	200	400	Ø	0%		

SHAFT RECYCLE AIR: 0% I.D. FAN % 56 SCRUBBER DP PERCENT OXYGEN: 5.3% DRAFT: - .35SHAFT RPM: 2.2 OPACITY: 5.12

TEST 4 4/5

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4/14/90 1645

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1284	1250	1	0%		
2	1260	1225	4	15%		
3	1591	1400	2	0%		
4	1612	1400	0	0%		
5	1309	1300	2	20%		
6	905	900	3	25%		
7	321	400	Ø	0%	100%	
8	200	400	Ø	0%		
9	200	400	Ø	0%		
10	200	400	Ø	0%	100%	
11	200	400	Ø	0%		

SHAFT RECYCLE AIR: 0 I.D. FAN % 54 SCRUBBER DP PERCENT OXYGEN: analyzed DRAFT: -1.35SHAFT RPM: 2.2 OPACITY: 4.89

TEST 3 5/5

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4/10/90 1700

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1372	1250	1	0%		
2	1311	1225	4	0%		
3	1741	1400	0	0%	30%	
4	1756	1400	0	0%		
5	1296	1300	2	55%		
6	908	900	3	30%		
7	325	400	Ø	0%	100%	
8	200	400	Ø	0%		
9	200	400	Ø	0%	100%	
10	200	400	Ø	0%		
11	200	400	Ø	0%		

SHAFT RECYCLE AIR: 0% I.D. FAN % 57 SCRUBBER DP

PERCENT OXYGEN: 7.3% DRAFT: -35

SHAFT RPM: 2.2 OPACITY: 5.51

TEST 3B 2/3

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4/10/90 1715

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1450	1250	1	0%		
2	1386	1225	4	0%		
3	1867	1400	0	0%	30%	
4	1821	1400	0	0%	5	
5	1256	1300	2	100%	30%	
6	906	900	3	30%		
7	311	400	0	0%	100%	
8	200	400	0	0%		
9	200	400	0	0%	100%	
10	200	400	0	0%		
11	200	400	0	0%		

SHAFT RECYCLE AIR: 0% I.D. FAN % 60% SCRUBBER DP

PERCENT OXYGEN: 7.6 DRAFT: -35

SHAFT RPM: 2.2 OPACITY: 4.8

TEST 3B

3/3

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4/10/90 1730

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1471	1250	1	0%		
2	1374	1225	4	0%		
3	1862	1400	0	0%	60%	
4	1850	1400	0	0%		
5	1262	1300	2	100%	60%	
6	879	900	3	60%		
7	299	400	Ø	0%	100%	
8	200	400	Ø	0%		
9	200	400	Ø	0%	100%	
10	200	400	Ø	0%		
11	200	400	Ø	0%		

SHAFT RECYCLE AIR: 0% I.D. FAN % 63% SCRUBBER DP _____

PERCENT OXYGEN: 10.4 DRAFT: -35

SHAFT RPM: 2.2 OPACITY: 5.38

Test 2 2/5

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4/10/90 1415

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1250	1220	1	2		
2	1248	1220	4	36		
3	1524	1420	2	2		
4	1580	1380	2	2		
5	1334	1220 900	2	58		
6	999	900	3	0		
7	4101	4100	0	2	80%	
8	253	380	0	0		
9	200	4100	0	0	80%	
10	202	380	0	0		
11	200			0		

SHAFT RECYCLE AIR: 0 I.D. FAN % ~~54~~ 54 SCRUBBER DP 8.36

PERCENT OXYGEN: 7.0 DRAFT: -35%

SHAFT RPM: 2.2 OPACITY: 5.64

TEST 2 3/5

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-10-90 1430

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1252	1220	Q 6	1		
2	1244	1220	36	4		
3	1404	1420	Q	2		
4	1524	1380	Q	Q		
5	1374	1320	58	2		
6	900	900	Q	3		
7	395	400	Q	Q	80%	
8	248	380	Q	Q		
9	200	400	Q	4	80%	
10	201	380	Q	Q		
11	200					

SHAFT RECYCLE AIR: Q I.D. FAN % 54 SCRUBBER DP 8.44

PERCENT OXYGEN: 7.4 DRAFT: -36

SHAFT RPM: 2.2 OPACITY: 5.55

4/10

13:30

1R

-7

1A

12:00:00

Stack Gas Opacity and Incinerator Exhaust
Oxygen Data - 4/10/90

stop @ 1245

1D

Oxygen
(%)

Opacity
(%)

TEST 1

1C

12:00:00

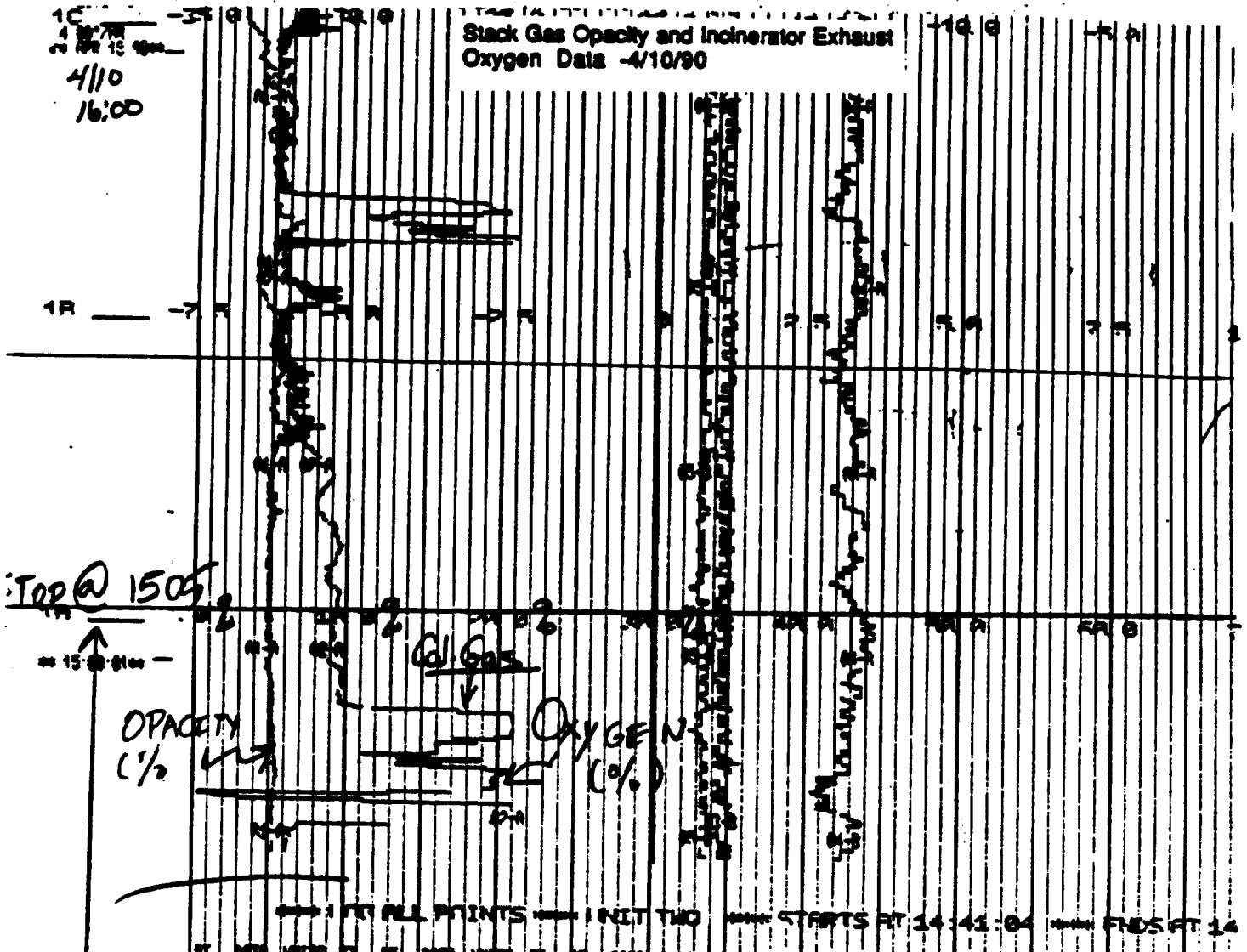
start
2 1138

11:30 AM
4/10

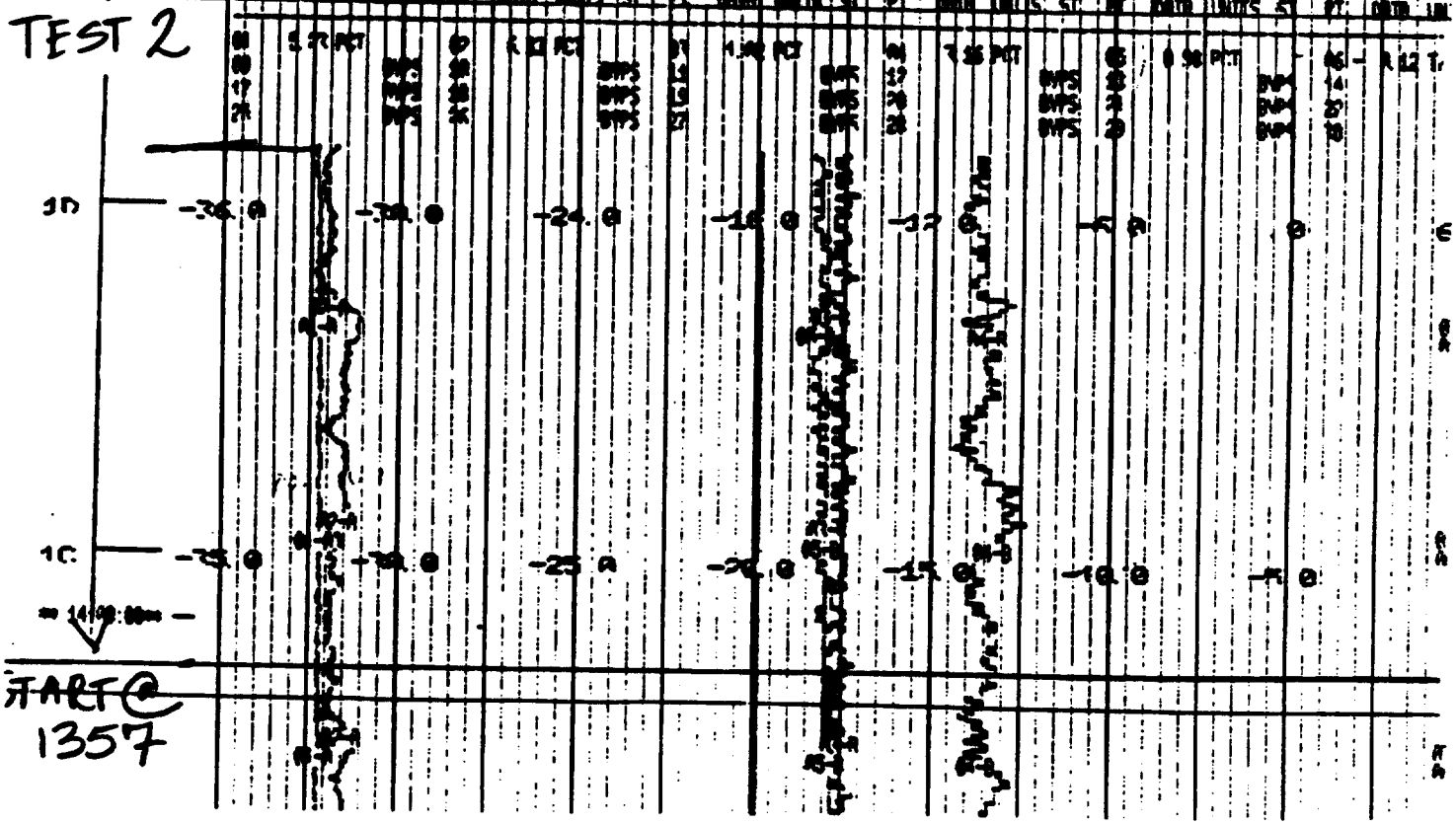
1B

1C
4/10
16:00

Stack Gas Opacity and Incinerator Exhaust Oxygen Data -4/10/90



TEST 2



**Incinerator Operating Data - Metals and
Hexavalent Chromium Tests
(4/11,12/90)**

SLUDGE FEED DATA SHEET

DATE: 4/1-90

Example Time	Feed Concentration 8% = .08	Constrate Concentration .4% = 0.004	Cake Concentration 20% = 0.20	Capture = (feed - constate) × cake (cake - constate) × feed $\frac{(.08 - .004) \times .20}{(.20 - .004) \times .08}$ = 0.95	Centri- fuge Flow gpm 85 gpm	Dry Furnace Feed = Flow × 0.34 × 60 × feed × capture $85 \times 0.34 \times 60 \times .08 \times .95$ = 2424 lb/hr	Wet Furnace Feed = Dry Feed cake $\frac{2424}{.20} = 0.323 \text{ lb/hr}$
2400	.047	.0010	.233	.48	76	1751	7517 (15,441)
		.0021	.208	.96	73	1648	7921
0200	.049	.0033	.215	.94	76	1765	8,209 (15,927)
		.0064	.208	.89	73	1605	7718
0400	.049	.0064	.239	.89	75	1652	6712 (15,500)
		.0028	.194	.95	73	1700	8,588
0600	.059	.0029	.244	.96	76	2159	8,849 (19,285)
		.0018	.242	.97	73	2108	10,434
0800		.0031	.227	.95%	74	1688	7438
		.0044	.206	.94%	74	1620	8110
1000		.0051	.223	.91%	76	1661	7449
		.0031	.193	.95%	73	1665 (1.66)	5670 (8.04)
1200		.0055	.231	.91%	75	1673	7244 (14,915)
		.0060	.210	.90%	73	1610 (1.64)	7671 (7.46)
1400		.0054	.232	.91%	71	1584	6828 (14,972)
		.0051	.200	.91%	73	1628 (1.61)	8144 (7.49)
1600	.040	.0049	.23	.90	75	1692	7359
		.0065	.20	.87	75	1632 (1.66)	8162 (15,521)
1800	.048	.0045	.23	.91	75	1632	7098 (7.78)
		.0062	.22	.87	75	1568	7130 (14,228)
2000	.045	.0045	.23	.90	75	1519	6608
		.0063	.22	.86	75	1452	6601 (13,209)
2200	.048	.0015	.23	.97	75	1745	7587
		.0058	.23	.88	75	1583	6885 (14,473)

M. M. H. 6
4 H. E. X. R.

M. M. H. 6
4 H. E. X. R.

SLUDGE FEED DATA SHEET

DATE: 4-12-90

	Food Concentration	Constrate Concentration	Sake Concentration	Capture = (food - contrate) = sake (sake - contrate) = food	Constrafe Flow gpm	Dry Furnace Food = Flow = 0.34 × 88 = food × capture	Wet Furnace Food = Dry Food sake
Example	0% = .00	1% = 0.004	20% = 0.20	$\frac{.00 - .004}{.20 - .004} = .05$ $\frac{.20 - .004}{.20 - .004} = .95$ = 0.05	85 gpm	$85 \times 0.34 \times 88 = .95 \times .95$ = 3024 lb/hr	$\frac{3024}{.95} = 3183 \text{ lb/hr}$
#1 #2 2400	.047	.0058 .0010	.235 .242	.89 .87	.65 .62	1373 1277	5,844 5280 (11,126)
0200	.047	.0010 .0021	.255 .216	.98 .96	.65 .62	1502 1406	5,890 6,612 (12,402)
0400	.049	.0028 .0017	.233 .222	.95 .97	.65 .62	1520 1478	6,527 6,461 (13,188)
0600	.051	.0045 .0037	.244 .239	.92 .94	.63 .65	1493 1562	6,118 6,535 (12,653)
0800		.0052 .0075	.247 .205	.92% .95%	.65 .62	1556 1532 3088	6299 2476 13,775 (6.89)
1000		.0027 .0038	.224 .220	.96% .94%	.65 .63	1592 1511 3103	6805 6486 13,281 (6.65)
1200		.0031 .0041	.238 .240	.95% .93%	.65 .62	1575 1471 3046	6621 6131 12,753 (6.38)
1400	.050	.0031 .0030	.250 .220	.95 .75	.65 .63	1545 1502 3047	6178 6827 13,006 (6.50)
1600	.051	.0032 .0039	.250 .240	.95 .94	.65 .63	1575 1509 3084	6700 6289 12,587 (6.29)
1800	.049	.0015 .0021	.260 .240	.98 .96	.65 .63	1546 1482 3028	5946 6179 12,125 (6.06)
2000	.051		.250 .230	.95 .95	.65 .63	1545 1527 3072	6180 6641 12,821 (6.41)
2200	.052		.250 .240	.93 .94	.65 .63	1512 1482	6150 6173 12,324

2-Minute
Max CR

PAH

PAH

#2 Furn

TEST 4 1/5

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-11-90 1030 Start

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1292	1200	1	0		
2	1275	1200	4	50		
3	1560	1400	0	0		
4	1604	1400	3	0		
5	1243	1250	0	0		
6	937	900	2	0		
7	466	400	2	0	70	
8	368	400	0	0	-	
9	353	400	1	0	70	
10	270	400	0	0	-	
11	200	-	-			

SHAFT RECYCLE AIR: 0 I.D. FAN % 52% SCRUBBER DP 7.57

PERCENT OXYGEN: ^{Being} ~~Spurred~~ DRAFT: .25

SHAFT RPM: 1.9 OPACITY: 4.5%

Phil Huntsman

TEST 4

2/5

#2

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-11-90 1100

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1289	1200	1	0		
2	1280	1220	4	50		
3	1521	1400	0	0		
4	1584	1400	3	0		
5	1210	1250	0	0		
6	937	900	2	0		
7	465	400	2	0	65	
8	334	400	0	0	—	
9	303	400	0	0	70	
10	261	400	0	0	—	
11	200	—	—	—	—	—

SHAFT RECYCLE AIR: 0 I.D. FAN % 52% SCRUBBER DP 7.50

PERCENT OXYGEN: ~~Being repaired~~ DRAFT: .24

SHAFT RPM: 1.9 OPACITY: 4.51%

Phil Hunterman

TEST 4

3/5

#2

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-11-90 1130

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1288	1200	1	0		
2	1279	1200	4	30		
3	1539	1400	0	0		
4	1589	1400	3	0		
5	1212	1250	0	0	—	
6	900	900	2	30	—	
7	437	400	2	0	65	
8	211	300	0	0	—	
9	200	200	0	0	65	
10	200	200	0	0	—	
11	200	—	—	—	—	

SHAFT RECYCLE AIR: 0 I.D. FAN % 51% SCRUBBER DP 7.43

PERCENT OXYGEN: ^{Being} ~~Revised~~ DRAFT: .23

SHAFT RPM: 1.9 OPACITY: —

4/5
TEST 4

#2

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-11-90 1200

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1278	1200	1	0		
2	1267	1200	4	50		
3	1516	1400	0	0		
4	1572	1400	3	0		
5	1205	1250	0	0		
6	905	900	2	50		
7	426	400	2	0	65	
8	200	400	0	0		
9	200	400	0	0	65	
10	200	400	0	0		
11	200	—	—	—	—	

SHAFT RECYCLE AIR: 0 I.D. FAN % 51% SCRUBBER DP 7.39

PERCENT OXYGEN: 5.3 DRAFT: .23

SHAFT RPM: 1.9 OPACITY: 4.72

TEST 4 5/5

#2
DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-11-90 1230

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1275	1200	1	0		
2	1265	1200	4	50		
3	1517	1400	0	0		
4	1573	1400	3	0		
5	1209	1250	0	0		
6	904	900	2	50		
7	429	400	2	0	65	
8	200	400	0	0	-	
9	200	400	0	0	65	
10	200	400	0	0		
11	200	—	—	—		

SHAFT RECYCLE AIR: 0 I.D. FAN % 50% SCRUBBER DP 7.41

PERCENT OXYGEN: 5.9 DRAFT: .23

SHAFT RPM: 1.9 OPACITY: 4.77

TEST 5 1/5

#2.

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-11-90 1415

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1291	1200	1	Ø		
2	1276	1200	4	90		
3	1533	14375	Ø	Ø		
4	1630	1400	3	Ø		
5	1433	14400	Ø	Ø		
6	1070	1100	2	Ø		
7	640	600	2	Ø	70	
8	249	400	Ø	Ø		
9	200	400	Ø	Ø	70	
10	200	400	Ø	Ø		
11	200	—	—	—	—	

SHAFT RECYCLE AIR: Ø I.D. FAN % 57% SCRUBBER DP 8.93

PERCENT OXYGEN: 6.6 DRAFT: .30

SHAFT RPM: 1.9 OPACITY: 5.05

#2

TEST 5 2/3

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-11-90 1445

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1228	1200	1	0		
2	1218	1200	4	30		
3	1522	1400	0	0		
4	1596	1400	3	0		
5	1370	1400	0	0		
6	1076	1100	2	80		
7	560	600	2	0	70	
8	220	400	0	0	-	
9	200	400	0	0	70	
10	200	400	0	0		
11	200	-	-	-	-	

SHAFT RECYCLE AIR: 0 I.D. FAN % 53% SCRUBBER DP 7.92

PERCENT OXYGEN: 5.3 DRAFT: -2.3

SHAFT RPM: 1.9 OPACITY: 5.0

TEST 5 ^{3/13}

#2

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-11-90 1515

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1236	1200	1	0		
2	1214	1200	4	20		
3	1560	1400	0	0		
4	1625	1400	3	0		
5	1374	1400	0	0		
6	1077	1100	2	100		
7	538	600	2	0	70	
8	200	400	0	0	-	
9	200	400	0	0	70	
10	200	400	0	0		
11	200	-	-	-		

SHAFT RECYCLE AIR: 0 I.D. FAN % 53 SCRUBBER DP 8.12

PERCENT OXYGEN: 4.8 DRAFT: 129

SHAFT RPM: 1.9 OPACITY: 5.04?

TEST 5 9/2

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4/11/90 1545

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1242	1200	1	0%		
2	1215	1200	4	25%		
3	1547	1400	0	0%		
4	1619	1400	3	0%		
5	1374	1400	0	0%		
6	1077	1100	2	100%		
7	525	400	2	100%	76%	
8	200	400	0	0		
9	200	400	0	0	76%	
10	200	400	0	0		
11	200	400	0	0		

SHAFT RECYCLE AIR: 0 I.D. FAN % 53 SCRUBBER DP

PERCENT OXYGEN: 4.9 DRAFT: -30

SHAFT RPM: 1.9 OPACITY: 4.96

TEST 5 ⁵/₅

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4/11/90 1415

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1230	1200	1	0%		
2	1216	1200	4	50%		
3	1520	1400	0	0%		
4	1599	1400	3	0%		
5	1352	1400	0	0%		
6	1037	1100	2	100%		
7	499	600	2	100%	70%	
8	200	400	0	0%		
9	200	400	0	0%	70%	
10	200	400	0	0%		
11	200	400	0	0%		

SHAFT RECYCLE AIR: 0 I.D. FAN % 54 SCRUBBER DP PERCENT OXYGEN: 6.3 DRAFT: -1.30SHAFT RPM: 1.9 OPACITY: 4.96

TEST 6 1/5

#2

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-12-90 0830

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1257	1200	1	0		
2	1217	1220	4	30		
3	1549	1400	0	0		
4	1628	1400	0	0		
5	1132	1400	0	0		
6	831	800	2	0		
7	420	400	2	0	90	
8	200	200	0	0		
9	200	200	0	0	90	
10	200	200	0	0		
11	200	—	—	—	—	

SHAFT RECYCLE AIR: 0 I.D. FAN % 56. SCRUBBER DP 8.47

PERCENT OXYGEN: 8.0 DRAFT: .31%

SHAFT RPM: 20 OPACITY: 5.16%

Phil Huntsman

TEST 6 2/5

#2

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-12-90 0900

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1259	1200	1	0		
2	1231	1220	4	30		
3	1582	1400	0	0		
4	1630	1400	0	0		
5	1120	1100	0	0		
6	798	800	2	0		
7	421	400	2	0	70	
8	200	200	0	0		
9	200	200	0	0	70	
10	200	200	0	0		
11	200		-	-	-	

SHAFT RECYCLE AIR: 0 I.D. FAN % 51% SCRUBBER DP 7.69

PERCENT OXYGEN: 6.4 DRAFT: .30 %

SHAFT RPM: 2.0 OPACITY: 4.96

Phil Hunter

TEST 6 3/5

#2

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-12-90 0930

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1276	1200	1	Ø		
2	1254	1220	4	Ø		
3	1661	1400	2	Ø		
4	1692	1400	Ø	Ø		
5	1090	1100	Ø	Ø		
6	776	800	2	Ø		
7	408	400	2	Ø	65	
8	200	200	Ø	Ø		
9	200	200	Ø	Ø	65	
10	200	200	Ø	Ø		
11	200	—	—	—		

SHAFT RECYCLE AIR: Ø I.D. FAN % 522 SCRUBBER DP 7.76

PERCENT OXYGEN: 4.9 DRAFT: .30

SHAFT RPM: 2.0 OPACITY: 4.85

Phil Huntman

TEST 6 4/3

#2

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-12-90 1000

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1300	1200	1	0		
2	1252	1220	4	0		
3	1606	1400	0	0		
4	1622	1400	0	0		
5	1094	1100	0	0		
6	780	800	0	0		
7	410	400	2	0	65	
8	200	200	0	0		
9	200	200	0	0	65	
10	200	200	0	0		
11	200	—	—	—	—	

SHAFT RECYCLE AIR: 0 I.D. FAN % 52 SCRUBBER DP 7.70

PERCENT OXYGEN: 8.0 DRAFT: .30

SHAFT RPM: 2.0 OPACITY: 4.80

TEST 6513

#2
DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-12-90 / 1030

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1246	1200	1	0		
2	1238	1220	4	60		
3	1396	1400	0	0		
4	1496	1400	0	0		
5	1038	1400	0	0		
6	720	800	0	0		
7	310	400	2	0	90	
8	200	200	0	0	—	
9	200	200	0	0	90	
10	200	200	0	0		
11	200	—	—	—	—	

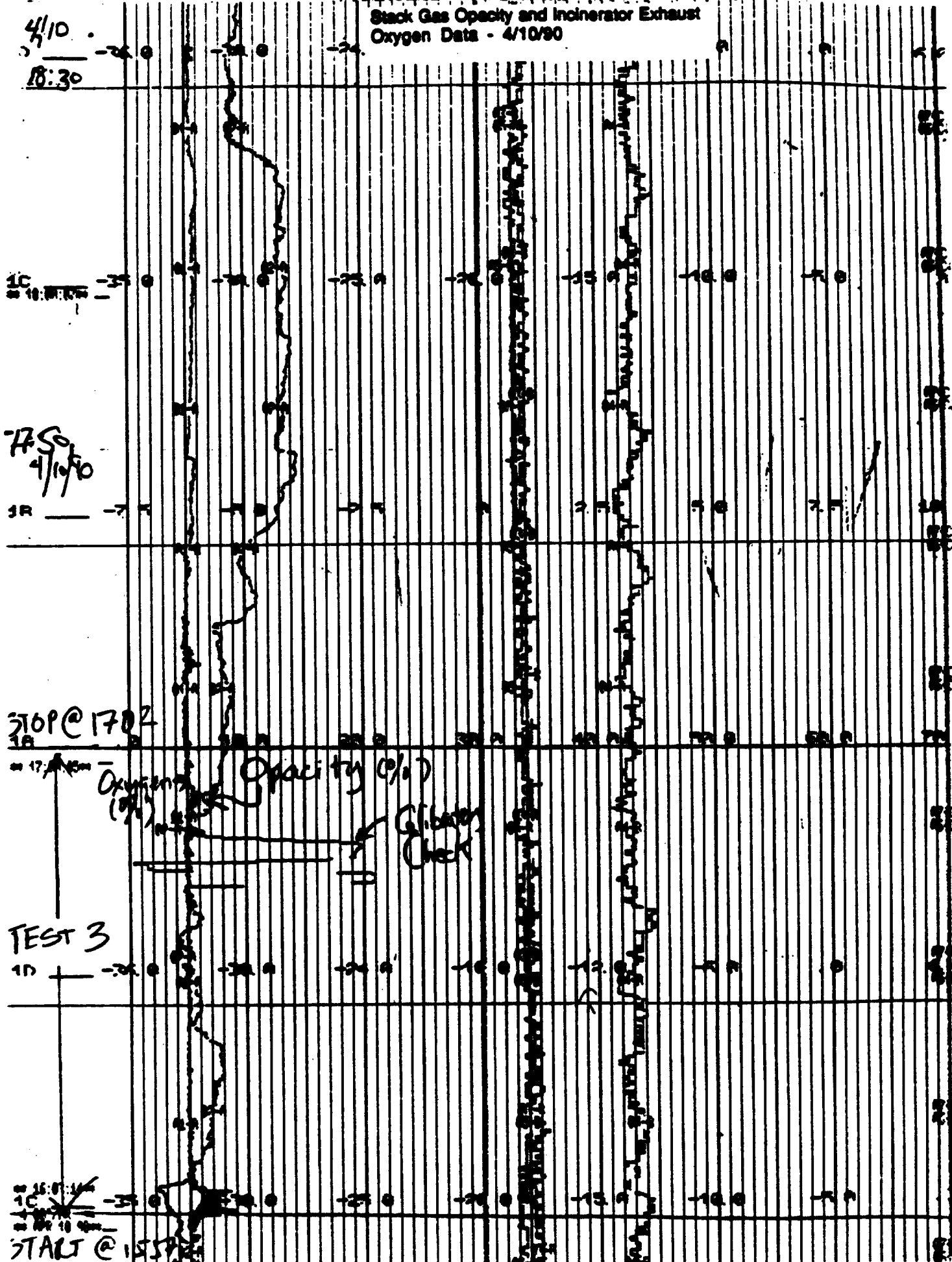
SHAFT RECYCLE AIR: 0 I.D. FAN % 53 SCRUBBER DP 7.96

PERCENT OXYGEN: 9.8 DRAFT: .31

SHAFT RPM: 2.0 OPACITY: 5.42

Phil Hunter

Stack Gas Opacity and Incinerator Exhaust
Oxygen Data - 4/10/90



Stack Gas Opacity and Incinerator Exhaust
Oxygen Data - 4/11/90

4/11

12:00

12:00

CONT 0

NEXT PAGE

1C

-3.2

-3.2

-2.5

-2.5

-2.5

-2.5

-2.5

-2.5

1R

-7.5

-7.5

-7.5

-7.5

-7.5

-7.5

-7.5

-7.5

TEST 4

OPACITY
(%)

1A

-3.2

-3.2

-2.5

-2.5

-2.5

-2.5

-2.5

-2.5

START 10 1027

1C

-3.2

-3.2

-2.5

-2.5

-2.5

-2.5

-2.5

-2.5

1C

-3.2

-3.2

-2.5

-2.5

-2.5

-2.5

-2.5

-2.5

1C

-3.2

-3.2

-2.5

-2.5

-2.5

-2.5

-2.5

-2.5

4/11/90 9:40

Stack Gas Opacity and Incinerator Exhaust
Oxygen Data - 4/11/80

4/11.

14:39 Cont'd
next page

TEST 5

START @

1410

14:00:00

1C

1B

12:00:00

1A

STOP @ 1243

1D

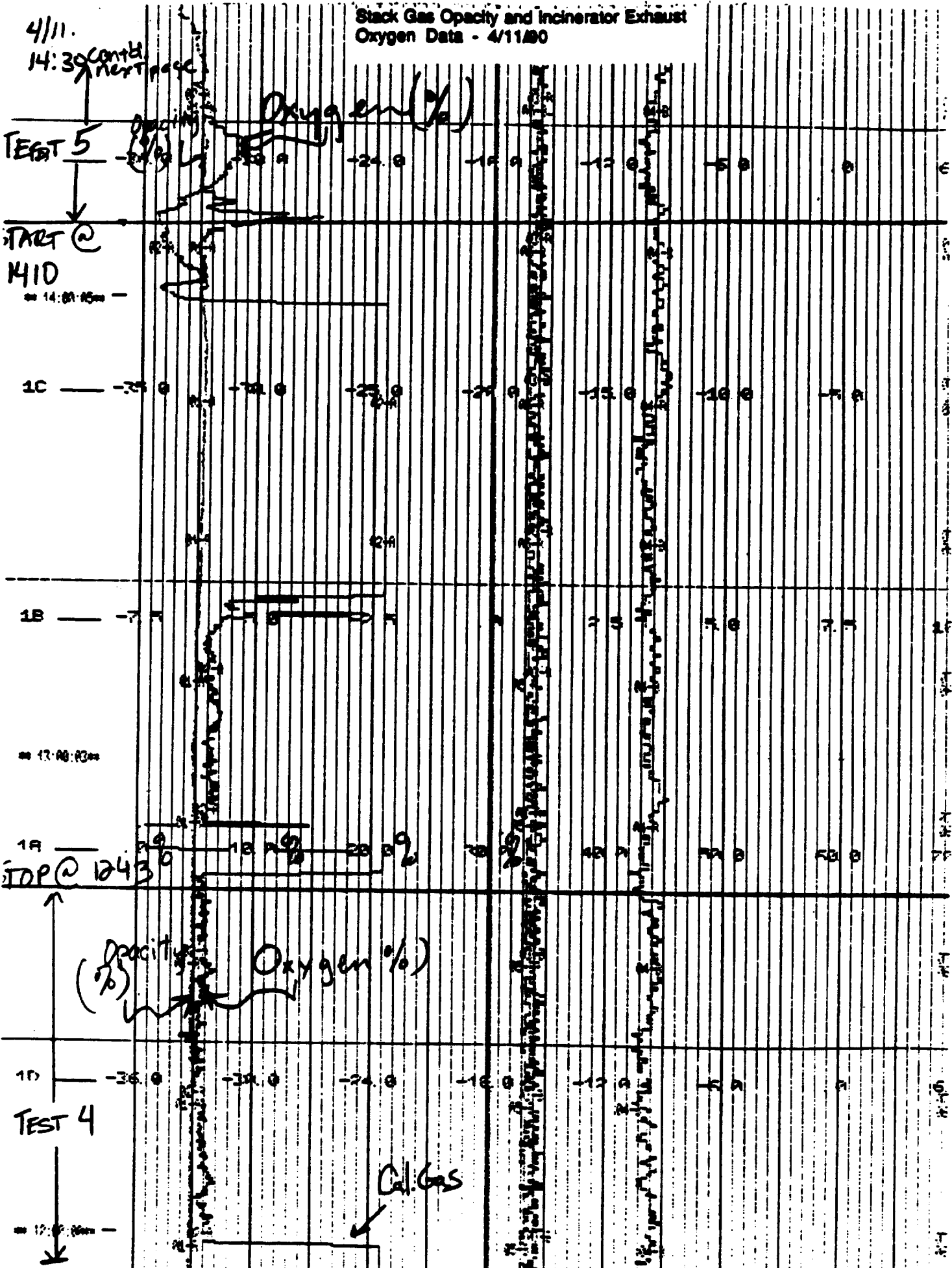
TEST 4

12:00:00

Oxygen (%)

(%) Opacity
Oxygen (%)

Cal Gas



[illegible]

Stack Gas Opacity and Incinerator Exhaust
Oxygen Data - 4/12/90

4/12
10:30

CONT'D
NEXT PAGE

10

10:30:00

10

TEST 6

10

10:30:00

START @
0833

4/12

10

10:30:00

Opacity
(%)

Oxygen
(%)

Calibration
Gas

FC

SA

FC

SA

FC

SA

FC

SA

FC

SA

FC

SA

4/12

13:00

1R

Stack Gas Opacity and Incinerator Exhaust
Oxygen Data - 4/12/90

TEST 7

START @
1219

1D

12:00:00

1C

12:00:00

1A

12:00:00

TOP @ 1052

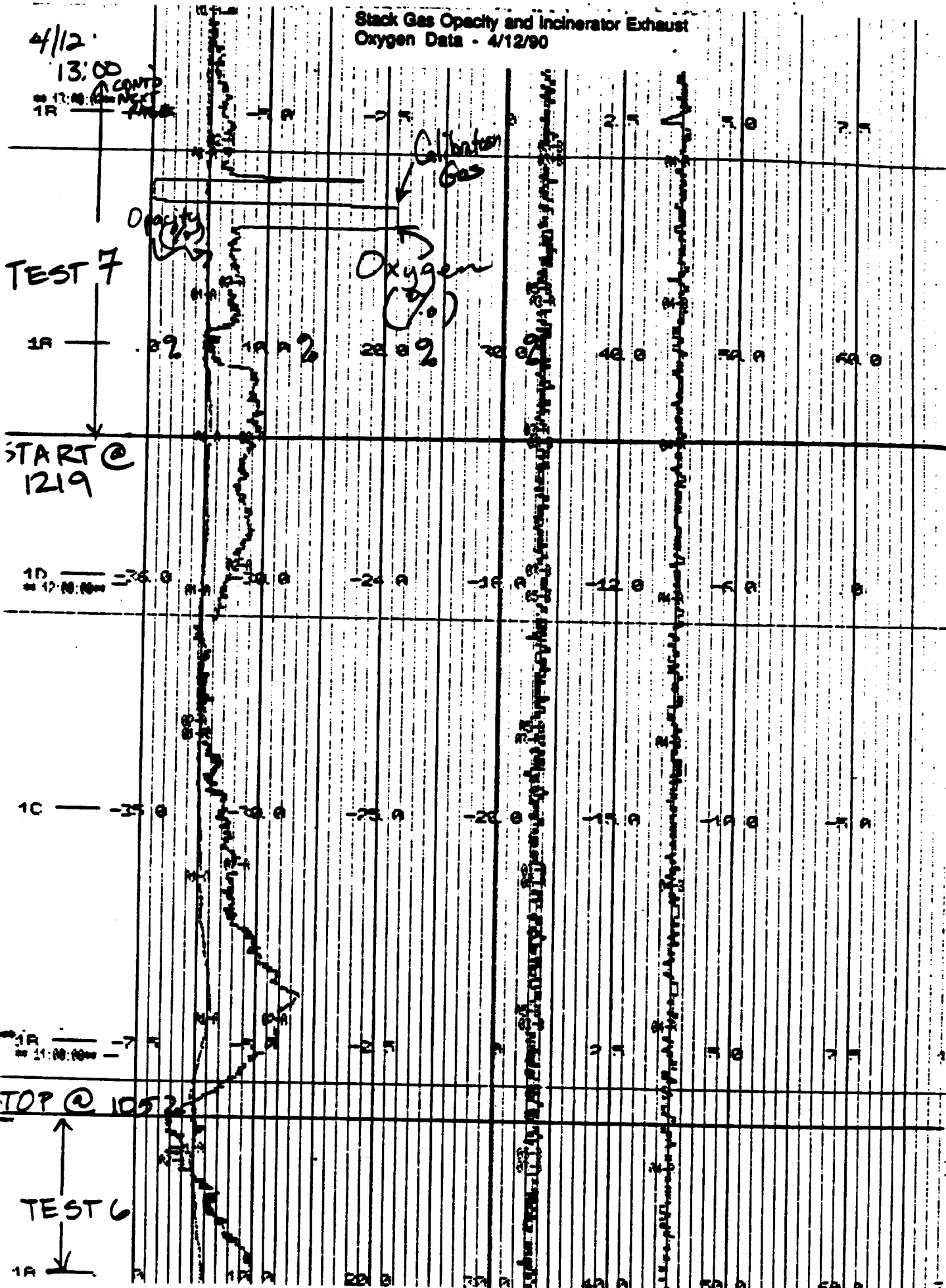
TEST 6

1A

Opacity

Oxygen
(%)

Calorifier
Gas



**Incinerator Operating Data - PCDD/PCDF and
PAH Tests (4/12,13/90)**

SLUDGE FEED DATA SHEET

DATE: 4-12-90

		Feed Concentration	Constrate Concentration	Cake Concentration	Capture = $\frac{(\text{feed} - \text{constrate}) \times \text{cake}}{(\text{cake} - \text{constrate}) \times \text{feed}}$	Constr- Flow gpm	Dry Furnace Feed = $\text{Flow} \times 8.34 \times 60 \times$ $\text{feed} - \text{capture}$	Wet Furnace Feed = $\frac{\text{Dry Feed}}{\text{cake}}$
Example		8% = .08	.4% = 0.004	20% = 0.20	$\frac{(0.08 - 0.004) \times .20}{(0.20 - 0.004) \times .08}$ = 0.95	85 gpm	$85 \times 8.34 \times 60 \times .08 = 2424 \text{ lb/hr}$	$\frac{2424}{.20} = 9,323 \text{ lb/hr}$
21 # 2	2400	.047	.0058	.235	.89	65	1373	5,846 (11,126)
	0200	.047	.0010	.242	.87	62	1277	5280 (12,402)
			.0021	.216	.96	62	1406	6,612 (13,188)
	0400	.049	.0028	.233	.95	65	1520	6,527 (13,188)
			.0017	.222	.97	62	1478	6,461 (12,653)
	0800	.051	.0045	.244	.92	63	1493	6,118 (12,653)
			.0037	.239	.94	65	1562	6,535 (12,653)
	0800		.0052	.247	.92%	65	1556	6299 (13,775)
4-Minute Hex (R)	2	.052	.0075	.205	.95%	62	1532 (1.54)	7476 (6.89)
	1000		.0027	.224	.96%	65	1592	6805 (13,281)
	2	.051	.0038	.220	.94%	63	1511 (1.55)	6486 (6.65)
	1200		.0031	.238	.95%	65	1575	6621 (12,752)
	2	.051	.0041	.240	.93%	62	1471 (1.52)	6131 (6.38)
1-PAH	1400	.050	.0031	.250	.95	65	1545	6178 (13,006)
	2		.0030	.220	.95	63	1502 (1.52)	6828 (6.50)
	1600	.051	.0032	.250	.95	65	1575	6300 (13,589)
			.0039	.240	.94	63	1509 (1.54)	6289 (6.24)
	1800	.049	.0015	.260	.97	65	1546	5946 (12,125)
-PAH			.0021	.240	.96	63	1482 (1.51)	6179 (6.06)
	2000	.051		.233	.95	65	1545	580 (12,821)
				.230	.95	63	1527 (1.54)	6641 (6.41)
	2200	.050		.250	.93	65	1532	5550 (12,224)
				.240	.94	63	1482	5731 (6.22)

SLUDGE FEED DATA SHEET

DATE: 4-13-90

	Food Concentration	Constrate Concentration	Cake Concentration	Capture = (food - constrate) = cake (cake - constrate) = food	Centrifuge Flow gpm	Dry Furnace Feed = flow = 8.34 × 80 × food = capture	Wet Furnace Feed = Dry Food cake
Example	8% = .08	4% = 0.004	20% = 0.20	$\frac{(0.08 - 0.004) \times 20}{(0.20 - 0.004) \times .08}$ = 0.96	85 gpm	$85 \times 8.34 \times 80 \times .08 \times .96$ = 2424 lb/hr	$\frac{2424}{.20} = 0.323 \text{ lb/hr}$
Time							
2400	.059	.0063	.247	.91	65	1758	7,121 (14,206)
		.0061	.234	.92	61	1657	7,085
0200	.052	.0038	.244	.94	65	1590	6,025
		.0037	.259	.94	61	1495	5,774 (11,799)
0400	.050	.0024	.228	.96	65	1564	6,862 (12,504)
		.0017	.263	.97	61	1483	5,642
0600	.053	.0038	.240	.94	68	1701	7,087
		.0070	.236	.94	70	1660	7,036 (14,123)
0800	.051	.0028	.2351	.96	64	1567	6393
2		.0052	.2160	.92	66	1549	7171 13,564
1000							
			BUS				
1200	.051	.0070	.2514	.95	67	1527 3050	6673 13,336
		.0070	.2094	.87	67	1521 (1.53)	2263 (6.67)
1400	.052	.0041	.2447	.93	63	1524 3058	6100 12,960
		.0077	.2484	.88	67	1534 (1.53)	6175 (6.48)
1600	.051	.0042	.241	.93	63	1495 3051	6244 12,504
		.0058	.246	.91	67	1536 (1.53)	6375 (6.25)
1800	.051	.0048	.232	.92	63	1526 3076	6377 13,114
		.0053	.230	.92	66	1550 (1.54)	6737 (6.56)
2000	.051	.0034	.234	.94	65	1559	6663
		.0035	.20.4	.94	66	1583	7068 13,131
2200	.051	.0028	.236	.95	66	1567	6448
		.0033	.218	.95	66	1569	7196 13,894

9-PAH

10-PAH

TEST 7 1/4

#2

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-12-90 1230

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1213	1200	1	0		
2	1205	1220	4	65		
3	1469	1400	0	0		
4	1527	1400	0	0		
5	1041	1400	0	0		
6	752	800	0	0		
7	360	400	2	0	70	
8	200	200	0	0		
9	200	200	0	0	70	
10	200	200	0	0		
11	200	—	—	—	—	

SHAFT RECYCLE AIR: 0 I.D. FAN % 51% SCRUBBER DP 2.80

PERCENT OXYGEN: 8.8 DRAFT: .29

SHAFT RPM: 2.0 OPACITY: 5.4

Phil Hunter

TEST 7 2/7

#2
DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-12-90 1300

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1230	1200	1	0		
2	1215	1220	4	25		
3	1545	1400	0	0		
4	1575	1400	0	0		
5	1110	1400	0	0		
6	780	800	0	0		
7	383	400	2	0	60	
8	200	200	0	0	-	
9	200	200	0	0	60	
10	200	200	0	0	-	
11	200	-	-	-	-	

SHAFT RECYCLE AIR: 0 I.D. FAN % 50% SCRUBBER DP 7.45

PERCENT OXYGEN: 6.5 DRAFT: .29

SHAFT RPM: 2.0 OPACITY: 4.83

Phil Hunterman

#2

TEST 7 3/7

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-12-90 1330

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1266	1200	1	0		
2	1215	1220	4	40		
3	1627	OFF	0	0		
4	1629	OFF	0	0		
5	1059	OFF	0	0		
6	766	800	0	0		
7	363	400	2	0	80	
8	200	OFF	0	0		
9	200	OFF	0	0	80	
10	200	OFF	0	0		
11	200	-	-	-		

SHAFT RECYCLE AIR: 0 I.D. FAN % 53 SCRUBBER DP 7.74PERCENT OXYGEN: 9.1 DRAFT: 30SHAFT RPM: 2.0 OPACITY: 565

#2

TEST 7 4/7

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-12-90 1400

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1210	1200	1	Ø		
2	1213	1220	4	48		
3	1441	OFF	Ø	Ø		
4	1509	OFF	Ø	Ø		
5	1006	OFF	Ø	2		
6	716	800	Ø	Ø		
7	327	400	2	Ø	80	
8	200	OFF	Ø	Ø		
9	200	OFF	Ø	Ø	80	
10	200	OFF	Ø	Ø		
11	200	—	—	—		

SHAFT RECYCLE AIR: 0 I.D. FAN % 52.9 SCRUBBER DP 7.72

PERCENT OXYGEN: 9.0 DRAFT: 31

SHAFT RPM: 2.0 OPACITY: 5.59

TEST # 5/7

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-12-90 1430

HEARTH NO.	TEMP.	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1212	1200	1	0		
2	1214	1220	3	100		
3	1458	1400	2	83		
4	1523	OFF	φ	φ		
5	1010	OFF	φ	2		
6	728	800	φ	φ		
7	324	400	2	φ	80	
8	200	OFF	φ	φ		
9	200	OFF	φ	φ	80	
10	200	OFF	φ	φ		
11	200	OFF	—	—		

SHAFT RECYCLE AIR: 0 I.D. FAN % 54.3 SCRUBBER DP 8.11

PERCENT OXYGEN: 7.1 DRAFT: 30

SHAFT RPM: 2.0 OPACITY: 538

TEST 7 6/4

42
DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-12-90 1500

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1300	1200	1	0		
2	1256	1220	3	100		
3	1650	1400	2	0		
4	1664	off	0	0		
5	1070	off	0	0		
6	747	800	0	0		
7	360	400	2	0	90	
8	200	200	0	0		
9	200	200	0	0	90	
10	200	off	0	0		
11	200	—	—	—	—	

SHAFT RECYCLE AIR: 0 I.D. FAN % 57% SCRUBBER DP 9.12

PERCENT OXYGEN: 8.6 DRAFT: 1.30

SHAFT RPM: 2.0 OPACITY: 6.1

Phil Huntman

#2

TEST 7 1/4

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-12-90 1530

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION %	COMMENTS
1	1208	1200	1	Ø		
2	1040	1200	3	100		
3	1380	OFF	—	Ø		
4	1438	OFF	—	Ø		
5	1107	OFF	—	Ø		
6	878	OFF	—	Ø		
7	523	700	2	120	60	
8	200	OFF	—	Ø		
9	200	OFF	—	Ø	45	
10	200	OFF	—	Ø		
11	200		—	Ø		

SHAFT RECYCLE AIR: Ø I.D. FAN % .25 SCRUBBER DP 6.87

PERCENT OXYGEN: 7.0 DRAFT: .25

SHAFT RPM: 2.0 OPACITY: 5.16 Rob Higgins

#2

TEST 8 1/4

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-12-90 1700

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1243	1200	1	0		
2	1148	1200	3	100		
3	1538	OFF	—	—		
4	1556	OFF	—	—		
5	1185	OFF	—	—		
6	924	OFF	—	—		
7	513	700	2	100	60	
8	200	OFF	—	—		
9	200	OFF	—	—	60	
10	200	OFF	—	—		
11	200	—	—	—		

SHAFT RECYCLE AIR: 0 I.D. FAN % 51.4 SCRUBBER DP 7.58

PERCENT OXYGEN: 3.7 DRAFT: .25

SHAFT RPM: 2.0 OPACITY: 4.76

Col Higgins

#2

TEST 8

2/7

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-12-90 1730

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1277	1200	1	Ø		
2	1135	1200	3	100		
3	1583	OFF	—	—		
4	1635	OFF	—	—		
5	1070	OFF	—	—	50	
6	758	OFF	—	—		
7	358	OFF	✓	—	100	
8	240	OFF	—	—		
9	336	500	2	100	100	
10	200	OFF	—	—		
11	200		—	—		

SHAFT RECYCLE AIR: Ø I.D. FAN % 564 SCRUBBER DP 8.65

PERCENT OXYGEN: 10.8 DRAFT: .26

SHAFT RPM: 1.8 OPACITY: 5.72 *Bob Higgins*

#2

TEST 8 34

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-12-90 1800

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1299	1200	1	Ø		
2	1256	1200	3	Ø		
3	1651	OFF	—	—		
4	1658	OFF	—	—		
5	1040	OFF	—	—	50	
6	846	OFF	—	—		
7	568	OFF	—	—	100	
8	602	600	2	100		
9	460	700	2	100	100	
10	255	OFF	—	—		
11	200	—	—	—		

SHAFT RECYCLE AIR: Ø I.D. FAN % 566 SCRUBBER DP 8.45

PERCENT OXYGEN: 2.2 DRAFT: 23

SHAFT RPM: 1.8 OPACITY: 4.81

Bob Higgins

#2

TEST 8

9/7

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-12-90 1830

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1204	1200	1	Ø		
2	1017	1200	3	100		
3	1376	OFF	—	—		
4	1421	OFF	—	—		
5	1045	OFF	—	—		
6	927	OFF	—	—		
7	460	OFF	—	—	50	
8	454	550	1	100		
9	461	500	2	52	50	
10	200	OFF	—	—		
11	200	—	—	—		

SHAFT RECYCLE AIR: Ø I.D. FAN % 49.4 SCRUBBER DP 6.92

PERCENT OXYGEN: 7.7 DRAFT: .23

SHAFT RPM: 1.8 OPACITY: 5.02 *Bob Higgins*

#2

TEST 8 5/4

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-12-90 1900

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1299	1200	1	0		
2	1201	1200	3	82		
3	1689	OFF	—	—		
4	1689	OFF	—	—		
5	1038	OFF	—	—	80	
6	828	OFF	—	—		
7	484	OFF	—	—	100	
8	418	550	1	100		
9	468	500	2	91	100	
10	259	OFF	—	—		
11	200	—	—	—		

SHAFT RECYCLE AIR: 0 I.D. FAN % 58 SCRUBBER DP 8.90

PERCENT OXYGEN: 8.9 DRAFT: .26

SHAFT RPM: 1.8 OPACITY: 5.76 *Rob Higgins*

#2

TEST 8 6/7

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-12-90 1930

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1260	1200	1	0		
2	1194	1200	3	100		
3	1566	OFF	—	—		
4	1618	OFF	—	—		
5	1038	OFF	—	—		
6	839	OFF	—	—		
7	495	OFF	—	—	90	
8	428	550	1	100		
9	463	500	2	75	90	
10	246	OFF	—	—		
11	200	—	—	✓		

SHAFT RECYCLE AIR: 0 I.D. FAN % 54.3 SCRUBBER DP 8.07

PERCENT OXYGEN: 5.6 DRAFT: .24

SHAFT RPM: 1.8 OPACITY: 5.05 Bob Higgins

II 2

TEST 8

9/9

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 4-12-90 2000

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1195	1200	1	10		
2	983	1200	3	100		
3	1315	OFF	—	—		
4	1378	OFF	—	—		
5	1011	OFF	—	—		
6	816	OFF	—	—		
7	478	OFF	—	—	40	
8	463	550	—	100		
9	485	500	—	30	40	
10	253	OFF				
11	200	—	—	—		

SHAFT RECYCLE AIR: 0 I.D. FAN % 45.5 SCRUBBER DP 6.12PERCENT OXYGEN: 6.5 DRAFT: .28SHAFT RPM: 1.8 OPACITY: 4.95*Bob Higgins*

(OVER)

Furnace has been smelted through-out the shift. Apparently coke is going from dry to moist enough to cause temps on upper hearth to increase & decrease considerably.

Tried switching from human on hearth #7 to one human on hearth #8 & 2 human on hearth #9. Didn't seem to help much. Basically increased & decreased input portions to Central Temp & Central oxygen during testing period.

4/12/90 (20:00)

TEST 9 1/8

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 1000 4-13-90

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1220	1200	1	Ø		
2	1040	1100	3	100		
3	1380	1400		85%		
4	1420	1450	2	85%		
5	1200	1320			66%	
6	970	1080				
7	660	800	2	100%	100%	
8	580	560	1	Ø		
9	600	500	2	Ø		
10	200	300				
11						

SHAFT RECYCLE AIR: ~~Ø~~ I.D. FAN % 53% SCRUBBER DP 8.0

PERCENT OXYGEN: 6.7 DRAFT: .23

SHAFT RPM: 1.7 OPACITY: 5.3

TEST 9 2/8

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 1030 4-8-80

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1260	1200	1	Ø		
2	1100	1100	3	40%		
3	1480					
4	1540	1450	2	Ø		
5	1220					
6	1000					
7	1080	800	2	100%		
8	600	560	1	Ø		
9	600	500	2	Ø		
10	200					
11						

SHAFT RECYCLE AIR: Ø I.D. FAN % _____ SCRUBBER DP _____

PERCENT OXYGEN: _____ DRAFT: _____

SHAFT RPM: 1.7 OPACITY: _____

TEST 9 3/8

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 11:00 4-13-90

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1260	1200	1		Ø	
2	1100	1100	3		78%	
3	1540					
4	1570	1450	2			
5	1200					
6	1000					
7	680	800	2		100%	
8	600	560	1			
9	610	500	2			
10	20					
11						

SHAFT RECYCLE AIR: Ø I.D. FAN % 52% SCRUBBER DP 7.9
 PERCENT OXYGEN: 5.4 DRAFT: .23
 SHAFT RPM: 1.7 OPACITY: 5.0

TEST 9 4/8

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 11:30 4-13-90

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1200	1200	1	Ø		
2	1020	1100	3	100%		
3	1390					
4	1420	1450	2	30%		
5	1200					
6	1000					
7	660	800	2	100%		
8	600	560	1	100%		
9	600	500	2	100%		
10	200					
11						

SHAFT RECYCLE AIR: Ø I.D. FAN % 57% SCRUBBER DP 7.6
 PERCENT OXYGEN: 5.8 DRAFT: .23
 SHAFT RPM: 1.7 OPACITY: 5.3

TEST 9 5/8

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 1200 4-13-90

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1290	1200	1	Ø	Ø	
2	1120	1100	3	Ø		
3	1530					
4	1560	1450	2	Ø		
5	1280				62	
6	1030					
7	680	800	2	100%	100%	
8	600	560	1	Ø		
9	600	500	2	Ø		
10	200					
11						

SHAFT RECYCLE AIR: Ø I.D. FAN % 52% SCRUBBER DP 7.6

PERCENT OXYGEN: 2.1 DRAFT: .23

SHAFT RPM: 1.7 OPACITY: 5.4

TEST 9 6/8

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 1230 4-13-90

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1260	1200	1	Ø	1.	
2	1070	1100	3	100%		
3	1480					
4	1500	1450	2	Ø		
5	1210				88%	
6	1010					
7	680	800	2	100%	100%	
8	600	560	1	Ø		
9	600	500	2	Ø		
10	200	500				
11						

SHAFT RECYCLE AIR: Ø I.D. FAN % 53 SCRUBBER DP 8.2

PERCENT OXYGEN: 7.3 DRAFT: 23

SHAFT RPM: 1.7 OPACITY: 5.4

TEST 9 7/8

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 1300 4-13-80

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1250	1200	1	Ø	Ø	
2	1100	1100	3	100		
3	1400					
4	1570	1450	2	Ø		
5	1200				70	
6	1000					
7	600	000	2	100	100	
8	600	500	1	Ø		
9	600	500	2	Ø		
10	200					
11						

SHAFT RECYCLE AIR: ~~Ø~~ I.D. FAN % 53 SCRUBBER DP 8.0
 PERCENT OXYGEN: 6.5 DRAFT: .23
 SHAFT RPM: 1.7 OPACITY: 5.4

TEST 9 8/8

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 1330 4-13-80

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENT
1	1220	1200	1	Ø		
2	1030	1100	3	100%		
3	1400					
4	1420	1450	2	20%		
5	1220				70%	
6	1000					
7	680	800	2	100%	100%	
8	600	560	1	Ø		
9	600	500	2	Ø		
10	200					
11						

SHAFT RECYCLE AIR: Ø I.D. FAN % 53% SCRUBBER DP 7.8

PERCENT OXYGEN: 6.4 DRAFT: 23

SHAFT RPM: 1.7 OPACITY: 5.5

TEST 10 1/0

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 1500 - 4-13-98

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1310	1200	1	Ø	Ø	
2	1180	1100	3	Ø		
3	1610					
4	1610					
5	1160				100%	
6	950					
7	680	800	2	100	100%	
8	600	560	1	Ø		
9	620	500	2	Ø		
10	200					
11						

SHAFT RECYCLE AIR: Ø I.D. FAN % 52. SCRUBBER DP 7.6

PERCENT OXYGEN: 5.7 DRAFT: .23

SHAFT RPM: 1.7 OPACITY: 4.9

TEST 10 2/8

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 1530 4-13-90

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1260	1200	1	Ø	Ø	
2	1080	1100	2	15		
3	1550					
4	1550	1450	2	Ø		
5	1150				76%	
6	950					
7	650	800	2	100	100%	
8	600	500	1	Ø		
9	600	500	2	Ø		
10	200					
11						

SHAFT RECYCLE AIR: Ø I.D. FAN % 52 SCRUBBER DP 7.5

PERCENT OXYGEN: 5.6 DRAFT: .23

SHAFT RPM: 1.7 OPACITY: 5.2

TEST 10 3/8

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME:

1600 - 41Z

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1204	1200	1	0		
2	1066		3	100	80	
3	1488		✓			
4	1500		✓			
5	1164		✓		80	
6	960		✓			
7	665		2	100	70	
8	602	550	1			
9	600	500	2			
10	200		0			
11						

SHAFT RECYCLE AIR: 0 I.D. FAN % 55 SCRUBBER DP 7.0

PERCENT OXYGEN: 6.5 DRAFT: .28

SHAFT RPM: 1.7 OPACITY: 5.4

TEST 10 4/8

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 1630 4-13

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1271	1200	1			
2	1174		3	0.	:	
3	1610		2		40	
4	1500		0			
5	1203		2		100.	
6	1017		0			
7	694		2	100%	100	
8	614	550	1			
9	636	500	2			
10	180		0			
11						

SHAFT RECYCLE AIR: 0 I.D. FAN % 55 SCRUBBER DP 2.2PERCENT OXYGEN: 45 DRAFT: 25SHAFT RPM: 1.7 OPACITY: 4.8

TEST 10 5/8

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 1700 4-13

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1188	1200	1			
2	1045		3	100%	25	
3	1518					
4	1540	1450				
5	1194	145			100	
6	1009					
7	905		2	100%	165	
8	671	550	1			
9	635	500	2			
10	181					
11	307					

SHAFT RECYCLE AIR: 0 I.D. FAN % 52 SCRUBBER DP 7.0

PERCENT OXYGEN: 10.0 DRAFT: 2.7

SHAFT RPM: 1.7 OPACITY: 5.6

TEST 10 6/8

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 1730 4-13-90

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1263		1	0		
2	1158		3	0.		
3	1612					
4	1616					
5	1215					
6	1043					
7	715		2	100%		
8	618		1	0		
9	638		2	0.		
10	179					
11	305					

SHAFT RECYCLE AIR: 0 I.D. FAN % 520/0 SCRUBBER OP 7.6PERCENT OXYGEN: 3.8 DRAFT: 1.23SHAFT RPM: 1.7 OPACITY: 49

TEST 10 7/8

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: ~~1800~~ 4-13-90

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1080		3			
2	1047			100%		
3	1462					
4	1486					
5	1193					
6	1008					
7	694		2	100%		
8	614		1			
9	639		2			
10	180					
11	301					

SHAFT RECYCLE AIR: 0 I.D. FAN % 52% SCRUBBER DP 7.6
 PERCENT OXYGEN: 8.3 DRAFT: 1.23
 SHAFT RPM: 1.7 OPACITY: 10.0

TEST 10 8/8

DATA SHEET FURNACE STACK EMISSIONS TESTING

DATE/TIME: 1800 4-13-90

HEARTH NO.	TEMP	TEMP SET POINT	NO. BURNERS ON	BURNER FIRING RATE	AIR PORT POSITION	COMMENTS
1	1002		0			
2	951		3			
3	1221					
4	1269					
5	1262				100%	
6	1040					
7	706		2	100%	100%	
8	619		1			
9	641		2			
10	200					
11	200					

SHAFT RECYCLE AIR: 0 I.D. FAN % 52 SCRUBBER DP 7.8PERCENT OXYGEN: 9.8 DRAFT: .21SHAFT RPM: 1.7 OPACITY: 6.8

4/12

13:00

1R

CONT'D
NEXT

Black Gas Opacity and Particulate Exhaust
Oxygen Data - 4/12/90

TEST 7

1R

29

19

20

20

20

20

20

20

20

20

20

20

20

20

START @
1219

1D

20

20

20

20

20

20

20

20

20

20

20

20

20

20

20

20

20

1C

20

20

20

20

20

20

20

20

20

20

20

20

20

20

20

20

20

1R

20

20

20

20

20

20

20

20

20

20

20

20

20

20

20

20

20

TOP @ 1052

TEST 6

Calibration Gas
Oxygen (%)

Stack Gas Opacity and Incinerator Exhaust
Oxygen Data - 4/12/90

4/12
15:00

15:00:00
1A

CONT'D
NEXT
PAGE

1A

Test 7

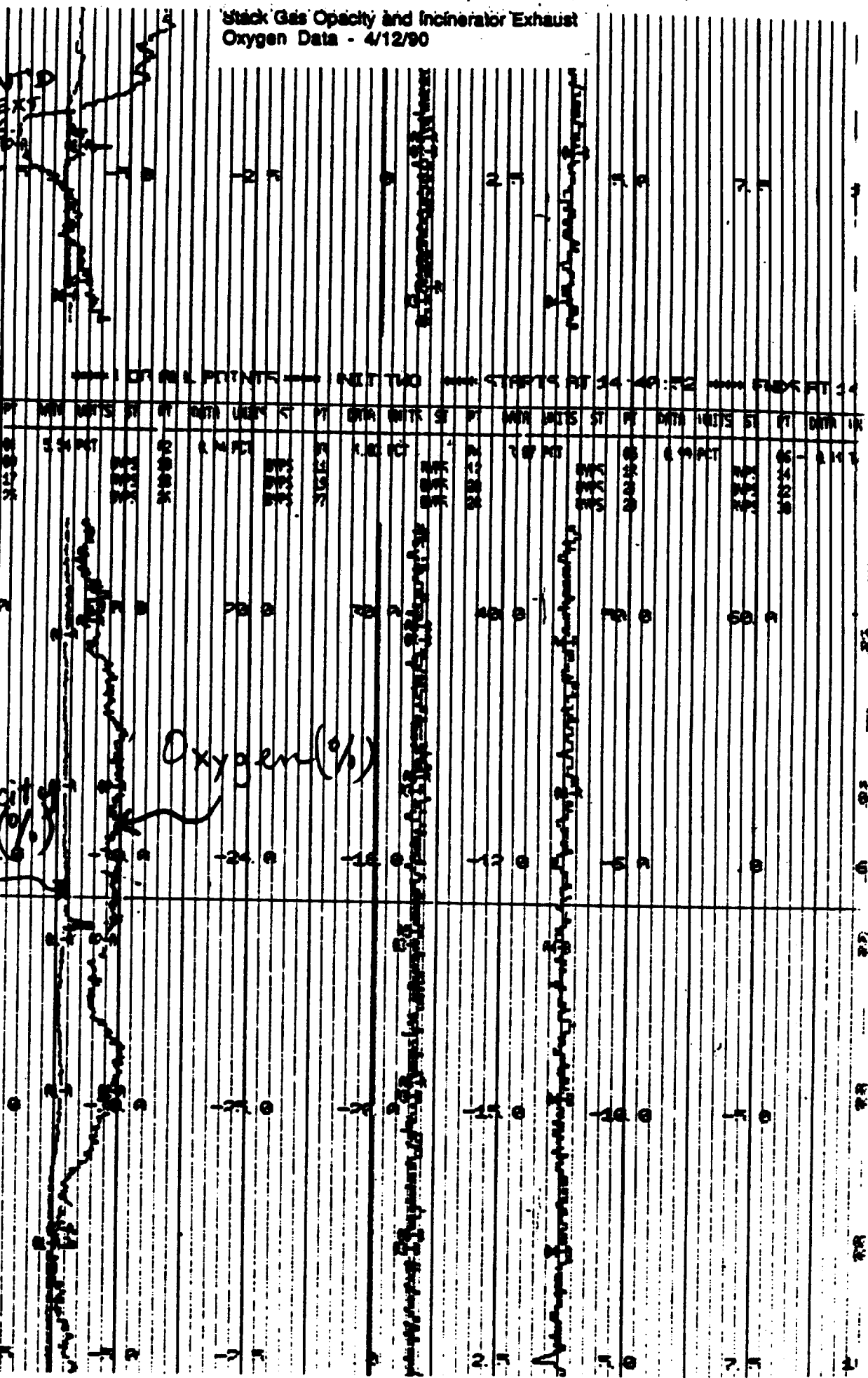
14:00:00
1B

1C

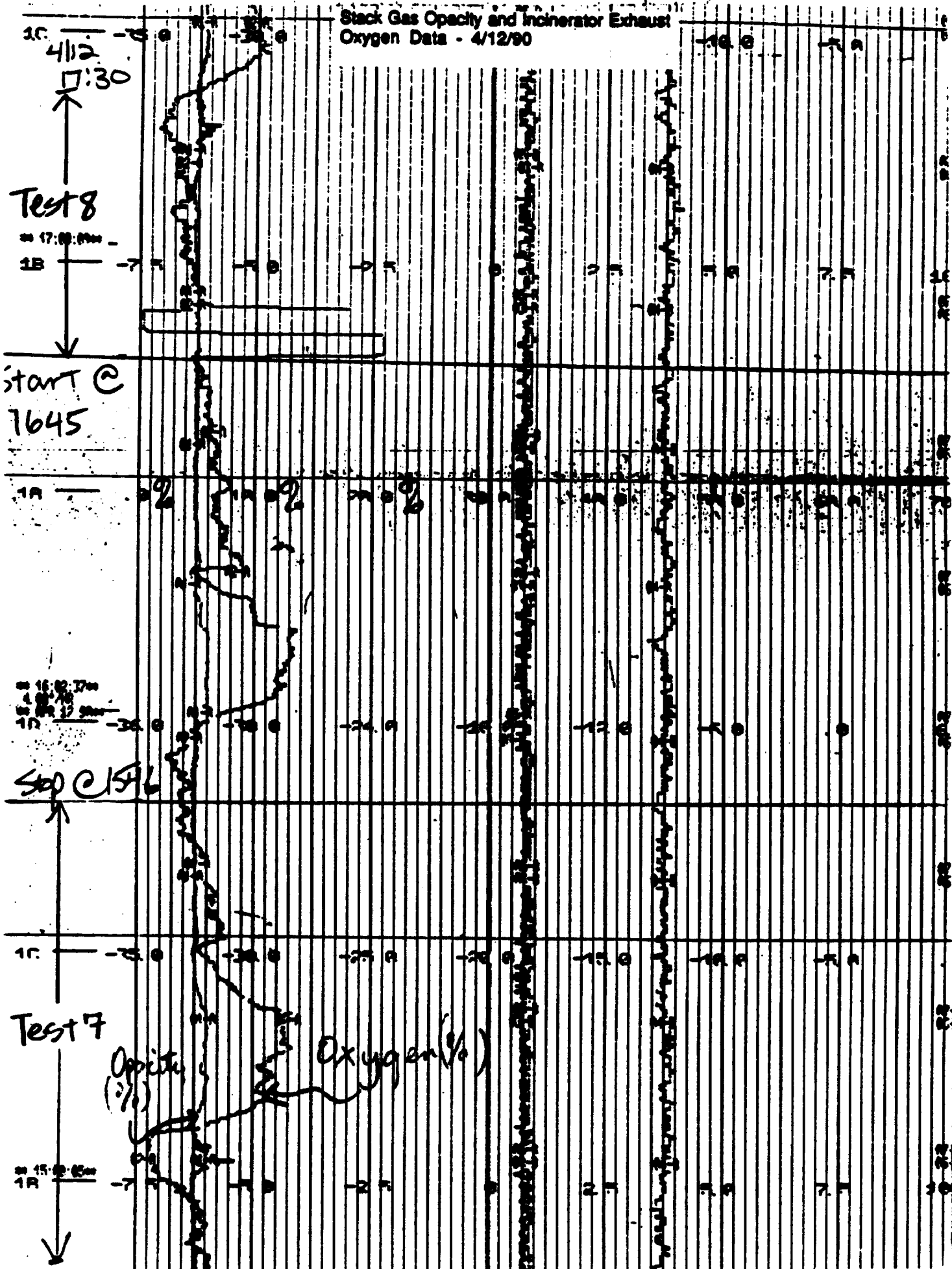
15:00:00
1D

Opacity (%)

Oxygen (%)



Stack Gas Opacity and Incinerator Exhaust
Oxygen Data - 4/12/90

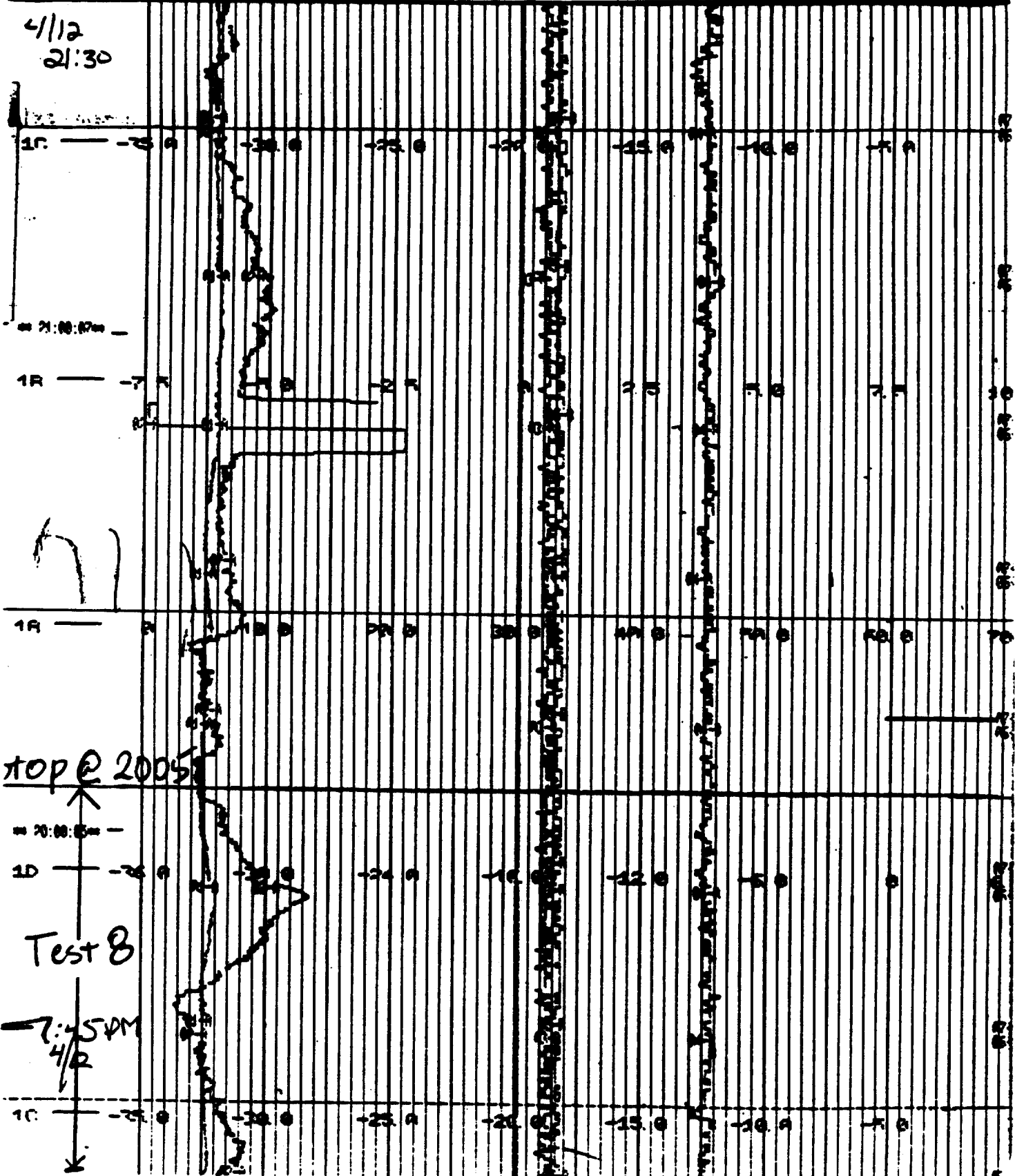


15.



Stack Gas Opacity and Incinerator Exhaust
Oxygen Data - 4/12/90

4/12
21:30



4/13 12:30

Stack Gas Opacity and Incinerator Exhaust
Oxygen Data - 4/13/90

1A CONT

12:00:00

10

-3

12

Cal Gas

TEST 9

10

-3

11:00:00

10

-3

10

START @

1010

10:00:00

10

-3

10

10

10

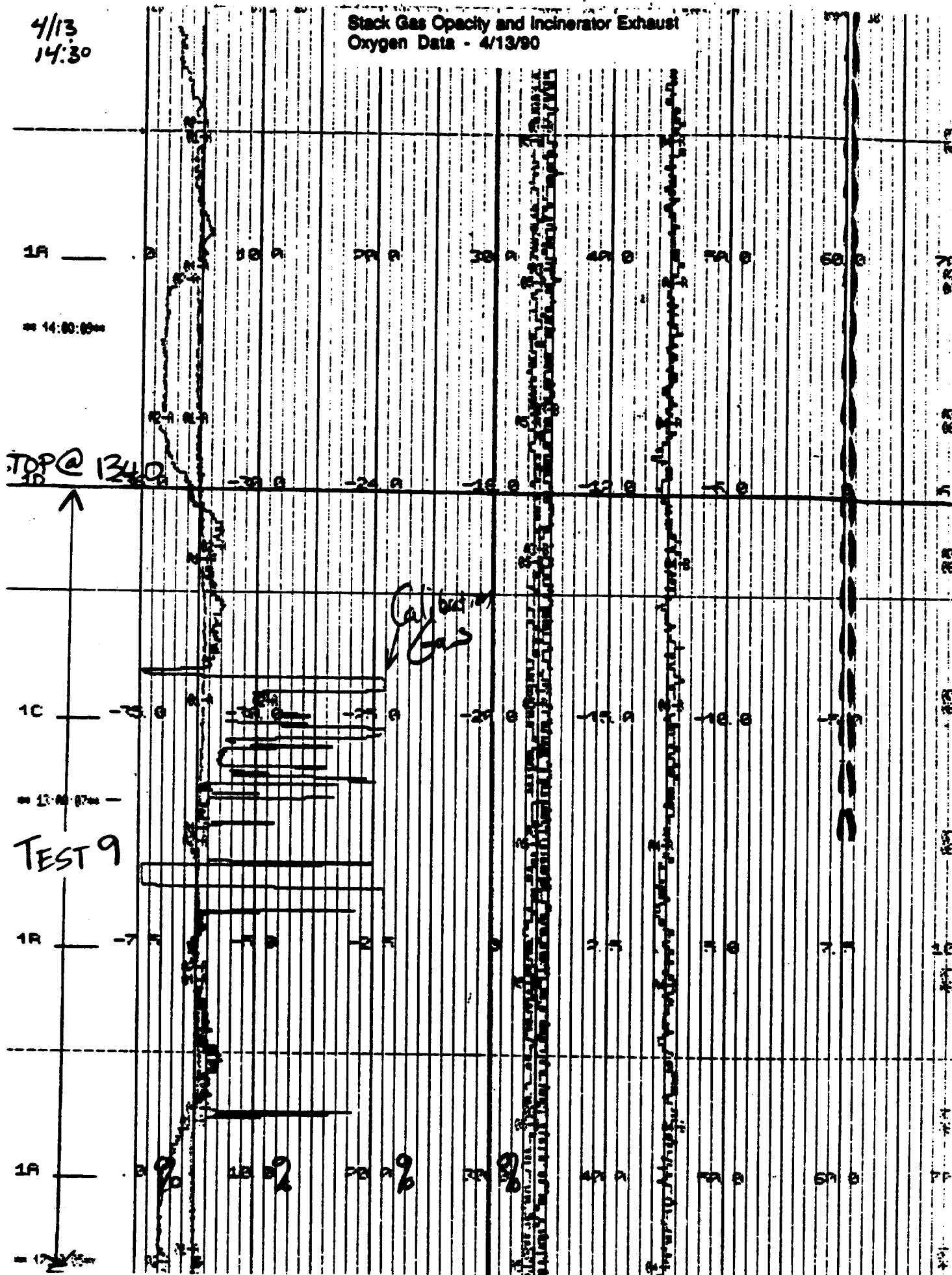
10

10

10

4/13
14:30

Stack Gas Opacity and Incinerator Exhaust
Oxygen Data - 4/13/90



4/13
16:30

Stack Gas Opacity and Incinerator Exhaust Oxygen Data - 4/13/80

Opacity (%) Oxygen (%)

Test 10

START
@ 1455

INITIAL POINTS				INITIAL TUN				STARTS AT 14:40				ENDS AT 14:45			
PT	DATA	UNITS	ST	PT	DATA	UNITS	ST	PT	DATA	UNITS	ST	PT	DATA	UNITS	ST
1	4.2	PCT	0	2	3.8	PCT	0	3	3.75	PCT	0	4	2.30	PCT	0
17	3.5	PCT	0	18	3.5	PCT	0	19	3.5	PCT	0	20	3.5	PCT	0
21	3.5	PCT	0	22	3.5	PCT	0	23	3.5	PCT	0	24	3.5	PCT	0

4/13

18:30

Stack Gas Opacity and Incinerator Exhaust
Oxygen Data - 4/13/90

STOP @ 823



1A

9%

9%

22%

30%

42%

5%

10%

18:04:04

10

-35%

-24%

1%

1%

4%

TEST 10

Opacity (%)

Oxygen (%)

15

-35%

-18%

-25%

-22%

1%

10%

1%

17:04:02

Calibration

1R

1%

10%

2%

1%

1%

1A

9%

12%

22%

30%

42%

5%

10%

APPENDIX II: STACK CONFIGURATION AND TRAVERSE POINT LOCATIONS

SELECTION OF SAMPLING SITES AND
NUMBER OF TRAVERSE POINTS
PARTICULATE TRAVERSES

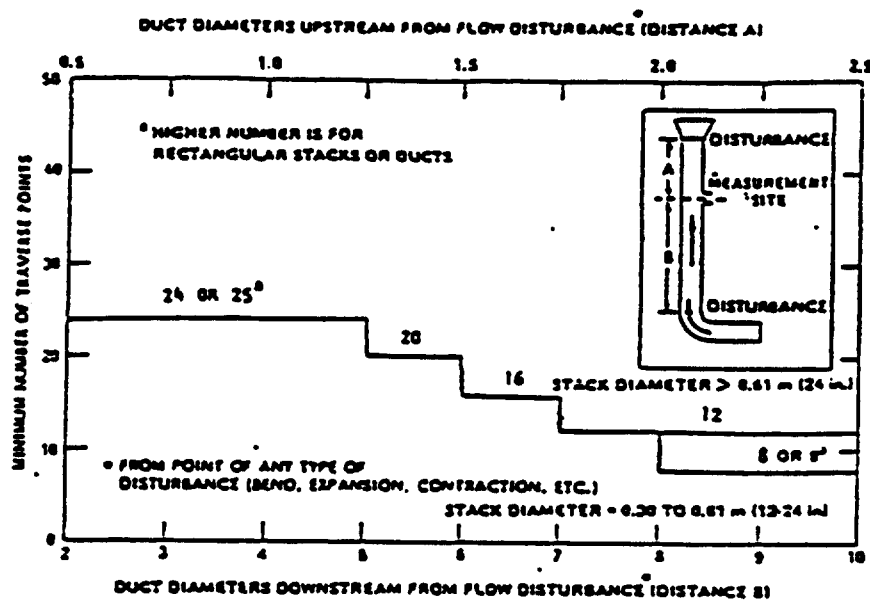


Figure 1-1. Minimum number of traverse points for particulate traverses.

[Method 1. — Figure 1-1 revised by 48 FR 45035, September 30, 1983]

Whenever sufficient straight stack or duct is available, the sampling site is located at least 8 stack diameters downstream and at least 2 stack diameters upstream from any flow disturbance such as a bend or an elbow or a fan. In situations where the above criteria cannot be met, the number of traverse points is increased according to the above graph.

For circular stacks, the traverse points are located on two diameters, the traverse axes dividing the stack cross-section into equal parts.

For rectangular stacks, the cross-section is divided into equal areas, such that the ratio of the length to width of the rectangles formed, is between 1 and 2. The traverse points are located at the center of each area.

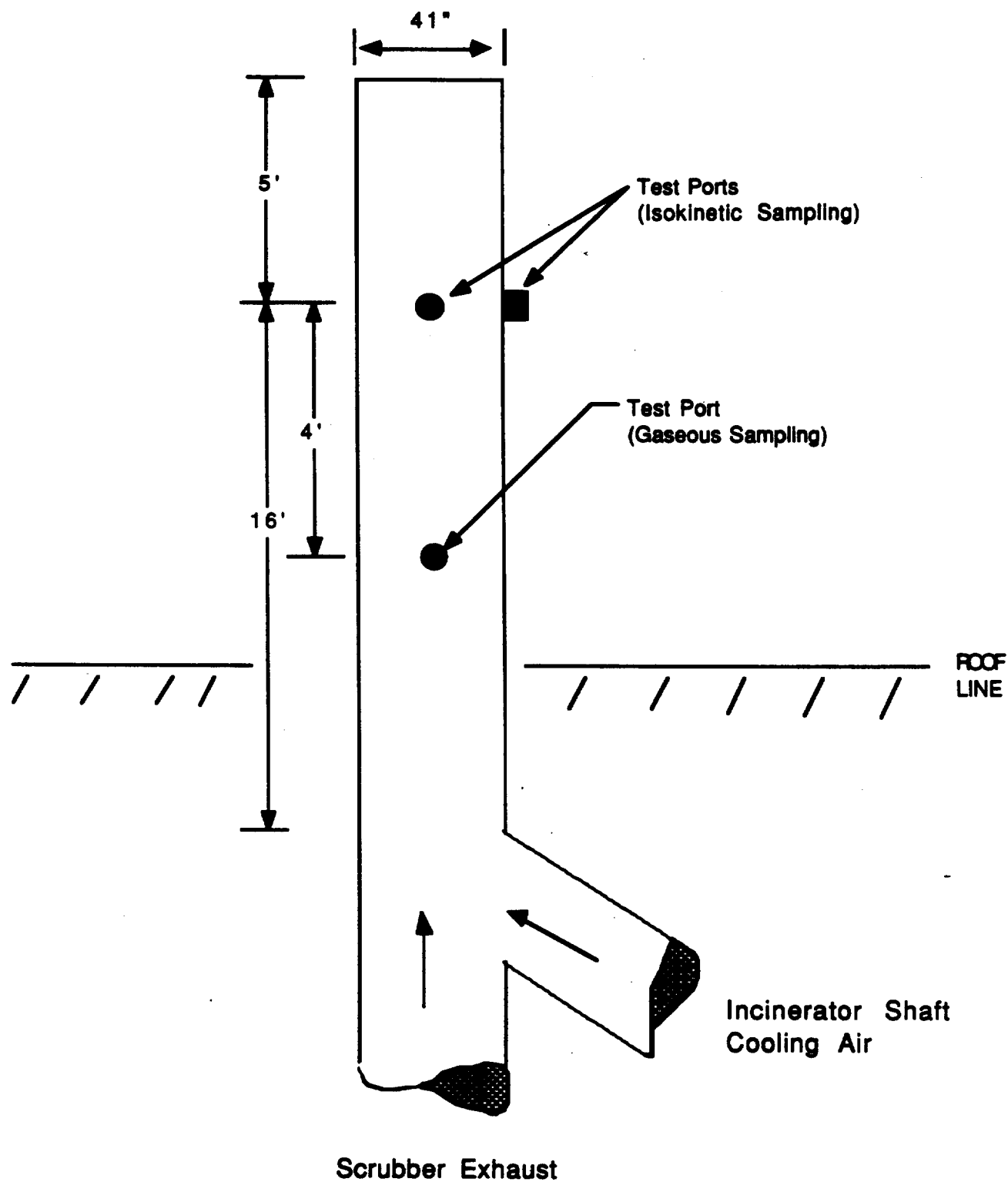
Traverse Point Locations (Circular Stack):

Stack Identification:	Incinerator #2 Exhaust
Stack Diameter:	41 inches
Sampling Locations:	4.7 diameters downstream 1.5 diameters upstream
Minimum Number of Traverse Points as Specified by CARB Method 1:	24
Number of Traverse Points Sampled:	24

Traverse Point Number	Distance From Inside Wall (Inches)
--------------------------	---------------------------------------

1	1.0 ¹
2	2.8
3	4.8
4	7.3
5	10.3
6	14.6
7	26.4
8	30.8
9	33.7
10	36.2
11	38.3
12	40.0 ¹

¹ Adjusted in accordance with CARB Method 1, Section 2.3.1.1.



Galson

Technical Services, Inc.
2116 Berkeley Way
Berkeley, CA 94704
Tel: (415) 848-0389
Fax: (415) 848-0838

SCALE:
N/A

JOB NUMBER:
SE-034

Central Contra Costa Sanitary District

File:
SE-034 THC

DATE:
9/6/90

DRAWN:
ML

Incinerator #2 Stack

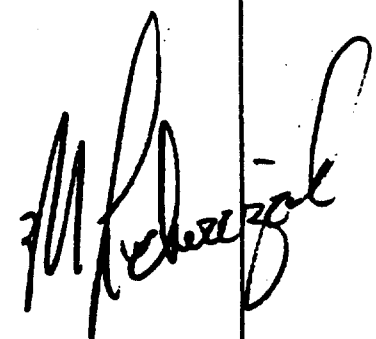
Disk:
SE034

CYCLONIC FLOW DETERMINATION

Plant: CCCSOStack: Unit #2 Stack

Traverse Point No.	Velocity Head ΔP , inches H_2O	Degrees Deviation From Reference α	Traverse Point No.	Velocity Head ΔP , inches H_2O	Degrees Deviation From Reference α
A3	1.10	0°			
A5	1.15	2°			
A8	0.95	1°			
A10	0.80	0°			
B3	1.15	1°			
B5	1.20	1°			
B8	0.95	3°			
B10	0.90	6°			

12/14/88

Average α = 1°

APPENDIX III: SAMPLING AND ANALYTICAL METHODS



6601 Kirkville Road
E Syracuse, NY 13057
Tel. (315) 432-0506
1-800-950-0506

LABORATORY ANALYSIS REPORT

Client: COCSD
Task Number: 90042315
Location: NS

Job Number: SE034LL
Date Sampled: 04/10-12/90

	Lab ID: J9299AC	J9299B	J9299D	J9299E		
	Client ID: TEST 6	TEST 6	TEST 6	TEST 6	TEST 6	
	CONTAINER A/C	CONTAINER B	CONTAINER D	CONTAINER E	TOTAL	
MERCURY	TOTAL UG	<0.8	1.3	24	260	285.3

Method(s): EPA DRAFT METHOD 8/28/89 METHOD EMISSIONS
FROM HAZARDOUS WASTE AND SIMILAR COMBUSTION
PROCESSES.

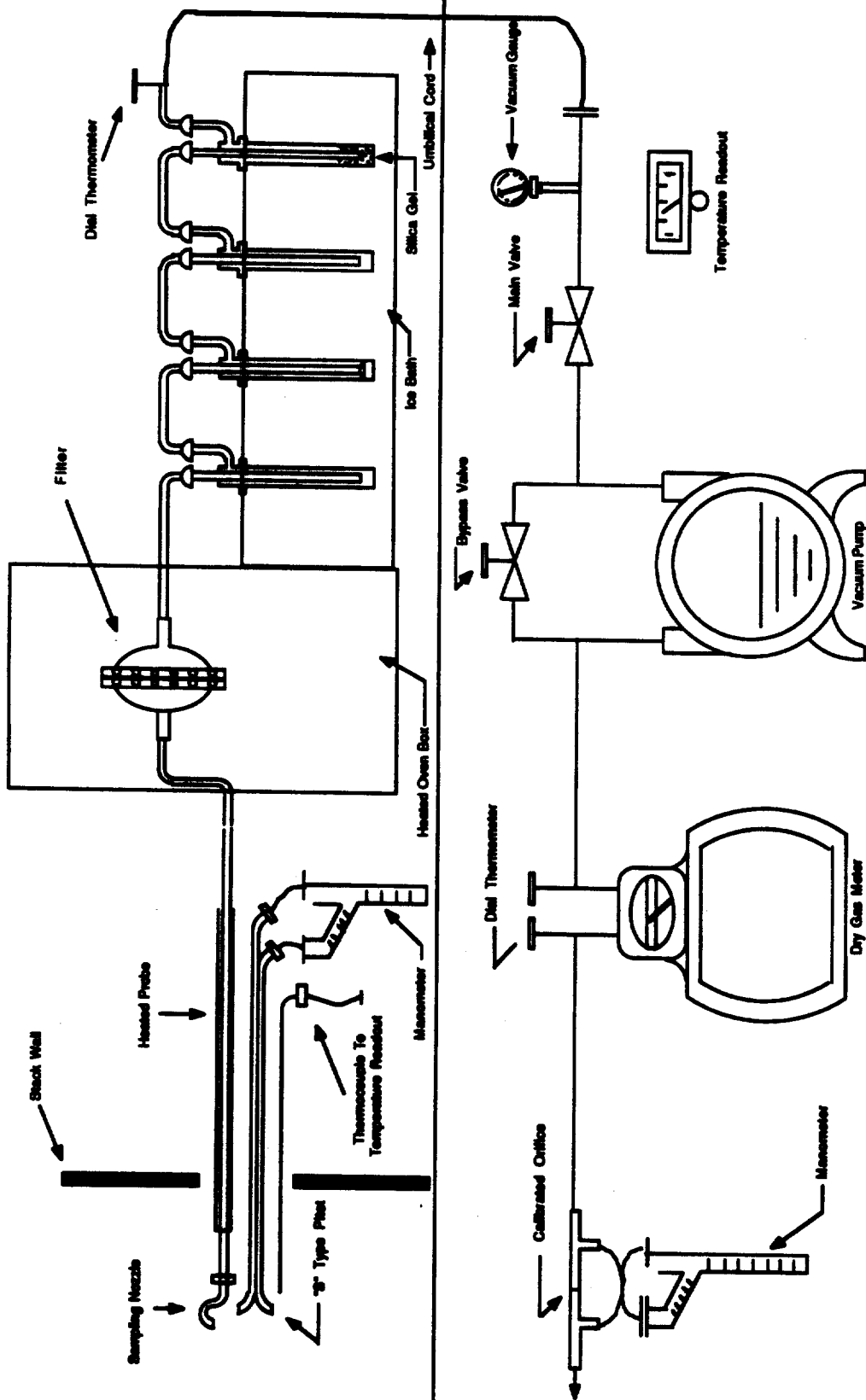
Footnotes: NO BLANK CORRECTIONS NEEDED.

(<) - Less Than
(>) - Greater Than
NA - Not Applicable
ND - Not detectable
NS - Not specified
MG - Milligrams
L - Liters
M³ - Cubic Meter
MG/M³ - Milligrams Per Cubic Meter
PPM - Parts Per Million
UG - Micrograms
NG - Nanograms
BL - Blank

Submitted by: ES, DS, PH

Approved by: *Mary E. Irthron*

Date: 4-MAY-1990



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Technical Services, Inc.
2116 Berkeley Way
Berkeley, CA 94704
Tel: (415) 849-0389
Fax: (415) 849-0838

SCALE: NA

DATE: 9/27/90

JOB NUMBER:
SE-034

DRAWN BY:
ML

CENTRAL CONTRA COSTA SANITARY DISTRICT

HCl SAMPLING SYSTEM

File:
HCl. Drawg

Disk:
SE034

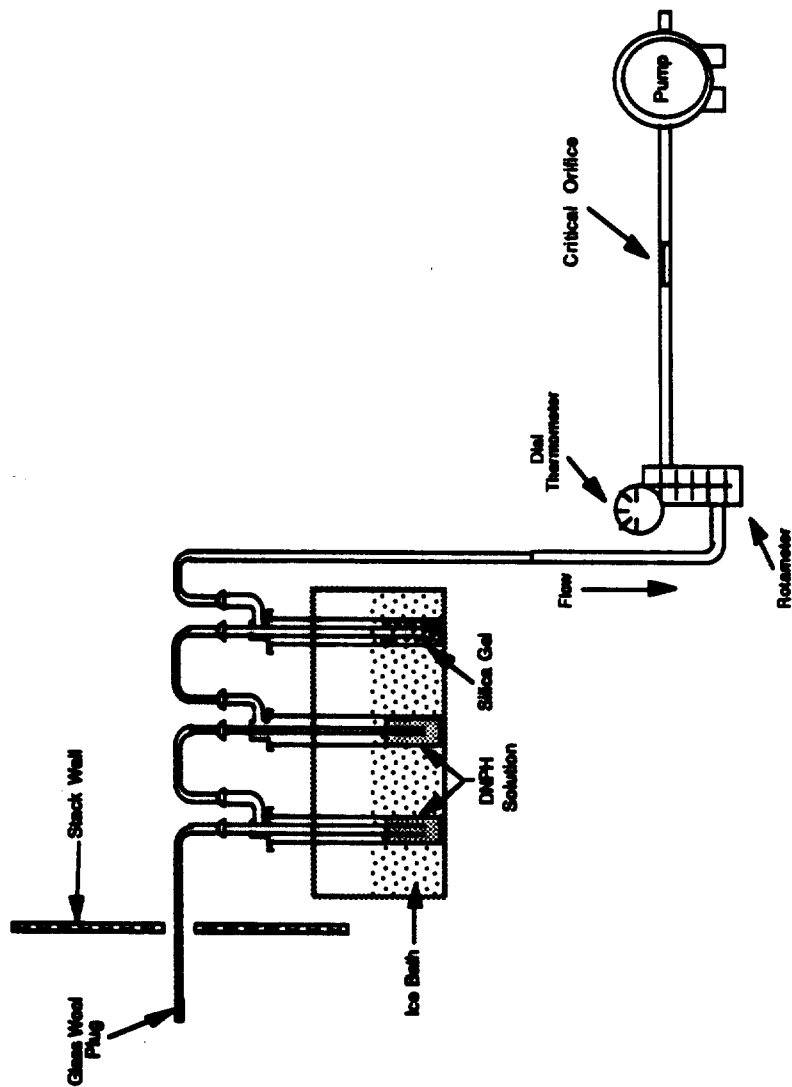
**SAMPLING AND ANALYTICAL METHODS:
FORMALDEHYDE EMISSIONS - CARB METHOD 430**

Formaldehyde emission testing was conducted in accordance with California Air Resources Board Method 430. The sampling train shown on the following page was utilized to collect the samples. Exhaust gases are drawn through a glass probe followed by two impingers containing 15 milliliters (each) of absorbing solution (2,4-dinitrophenylhydrazone, DNPH). Sample flow rate is regulated by a critical orifice/high vacuum pump assembly.

The DNPH solution is formulated within 48 hours of sampling. Sampling is performed at a single point in the exhaust stack/duct at a constant flow rate (i.e., approximately 1.0 liter per minute). The sampling rate is determined prior to each test period with a soap bubble flow meter; sample gas temperatures (at the critical orifice), rotameter readings, and pump vacuum are recorded at approximately 5 to 10 minute intervals during the testing.

At the end of the test interval, the sampling rate is again determined with the bubble meter. The solution is then transferred to a sample bottle, along with a small volume of rinse (approximately 5 milliliters of the DNPH). The samples are packaged (on ice) for shipment to the laboratory.

In the laboratory, the solution is extracted and the derivative is analyzed using high performance liquid chromatography (HPLC), coupled with ultraviolet (UV) absorption detector (at 360 nanometers). Quantification is provided by comparing the sample response with laboratory-prepared standards of formaldehyde. A field blank is prepared and analyzed in conjunction with the samples to determine if sample contamination occurred. The samples are extracted within seven days of collection.



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 Technical Services, Inc.
 2118 Berkeley Way
 Berkeley, CA 94704
 Tel: (415) 848-0060
 Fax: (415) 848-0030

SCALE: NA

DATE: 6/14/90

JOB NUMBER: SE-034

DRAWN BY: ML

CENTRAL CONTRA COSTA SANITARY DISTRICT

FORMALDEHYDE SAMPLING TRAIN

File: Form. Drwg

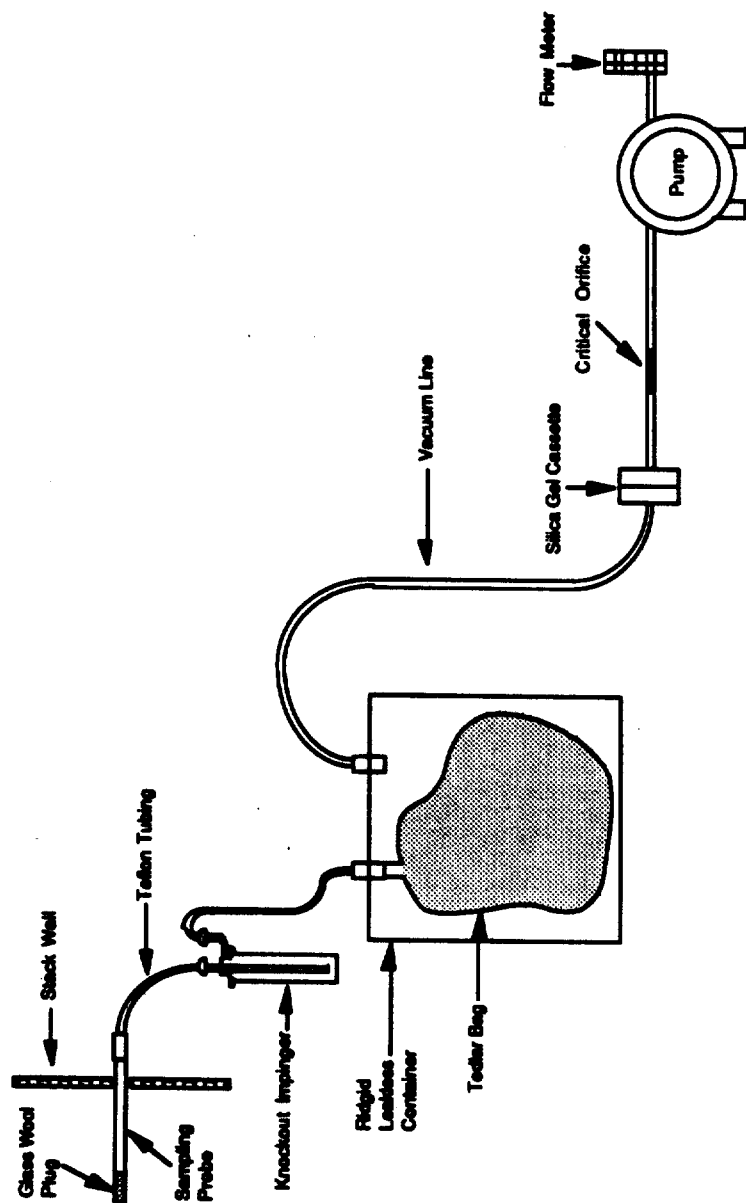
Disk: SE034

**SAMPLING AND ANALYTICAL METHODS:
BENZENE AND VINYL CHLORIDE EMISSIONS -
CARB METHODS 410A AND 106**

Benzene and vinyl chloride emission testing was conducted in accordance with California Air Resources Board Methods 410A and 106, respectively. The sampling train shown on the following page was utilized to collect the samples.

An integrated sample of the exhaust gas is collected in a tedlar bag. Sample gas is drawn through a stainless steel probe/integrated particulate filter (glass wool plug) assembly and through an empty impinger which serves to condense moisture. The gas then passes through teflon tubing and into a 10-liter tedlar bag. The bag is retained in a rigid, leak-free container (i.e., lung sampler) which is evacuated at a constant rate of approximately 0.2 lpm. The sampling system is leak tested prior to use.

Following sampling, the bag is labelled, sealed, and transferred to a storage container. Exposure to sunlight is minimized. The sample is then transferred to a laboratory where it is analyzed for benzene and vinyl chloride using gas chromatography/mass spectrometry (GC/MS). Quantification is provided by comparing the sample response with laboratory-prepared standards. A field blank (nitrogen) is prepared and analyzed in conjunction with the samples to determine if sample contamination occurred. Sample analyses are performed within 48 hours of collection.



GALSON Technical Services, Inc. 2116 Berkeley Way Berkeley, CA 94704 Tel: (415) 848-0388 Fax: (415) 848-0838	SCALE: NA DATE: 9/27/90	JOB NUMBER: SE-034 DRAWN BY: ML	CENTRAL CONTRA COSTA SANITARY DISTRICT BENZENE/VINYL CHLORIDE SAMPLING TRAIN (CARB 410A)	File: Benz/Vyl Cl. Drwg Desk: SE034
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**SAMPLING AND ANALYTICAL METHODS:
DETERMINATION OF PARTICULATE AND METALS (11) EMISSIONS -
EPA MULTIPLE METALS METHOD (DRAFT: 8/28/89)**

Particulate and metals emission testing was performed in accordance with the Environmental Protection Agency (EPA) Draft Multiple Metals Method (dated August 28, 1989), respectively. Sampling equipment manufactured by Research Appliance Corporation (RAC) and Nutech Corporation was utilized to collect the samples. A schematic of the sampling train is shown on the following page. Velocity pressure of the stack gas is measured with a Stausscheibe-type pitot tube connected to an inclined gauge manometer. Isokinetic sampling rates are calculated using a nomograph and sample flow rate is regulated accordingly by adjusting the pressure drop across a calibrated orifice. Total sample volume is measured with a dry gas meter. Direct thermocouple read-out is provided for stack gas, impinger effluent, probe, sampling box, and gas meter influent and effluent temperatures. Emissions of the following metals were determined:

Arsenic	Beryllium
Cadmium	Chromium (Total)
Copper	Lead
Manganese	Mercury
Nickel	Selenium
Zinc	

Stack gases are drawn through a glass nozzle and a heated, glass-lined sampling probe, prior to passing through a pre-weighed, 85 millimeter glass fiber filter (for particulate collection). The filter, which meets CARB specifications for removal efficiency, is maintained at 250°F. The gases are then bubbled through a series of five impingers in an ice bath. The first two impingers each contain 100 milliliters (mls) of a nitric acid/hydrogen peroxide solution¹; the third impinger is empty; the fourth impinger contains 100 mls of a potassium permanganate/sulfuric acid solution²; the fifth impinger contains 200 grams of indicating-type silica gel.

Following the completion of sampling, the filter is recovered and transferred to a storage container (Container C); the probe, nozzle, and filter holder are rinsed (and brushed) with acetone (Container A), and then rinsed (only) with the nitric acid/hydrogen peroxide solution (Container B). The volume of solution in the first, second, and third impingers is measured and transferred to Container D; these impingers (and connecting glassware) are then rinsed with the nitric acid/hydrogen peroxide solution and the rinses are added to Container D. The volume of solution in the fourth impinger is measured and transferred to Container E; this impinger is then rinsed with the potassium permanganate/sulfuric acid solution and transferred to Container E. Lastly, the silica gel in the fifth impinger is transferred to Container F.

¹ 5% HNO_3 /10% H_2O_2 .

² 4% KMnO_4 /10% H_2SO_4

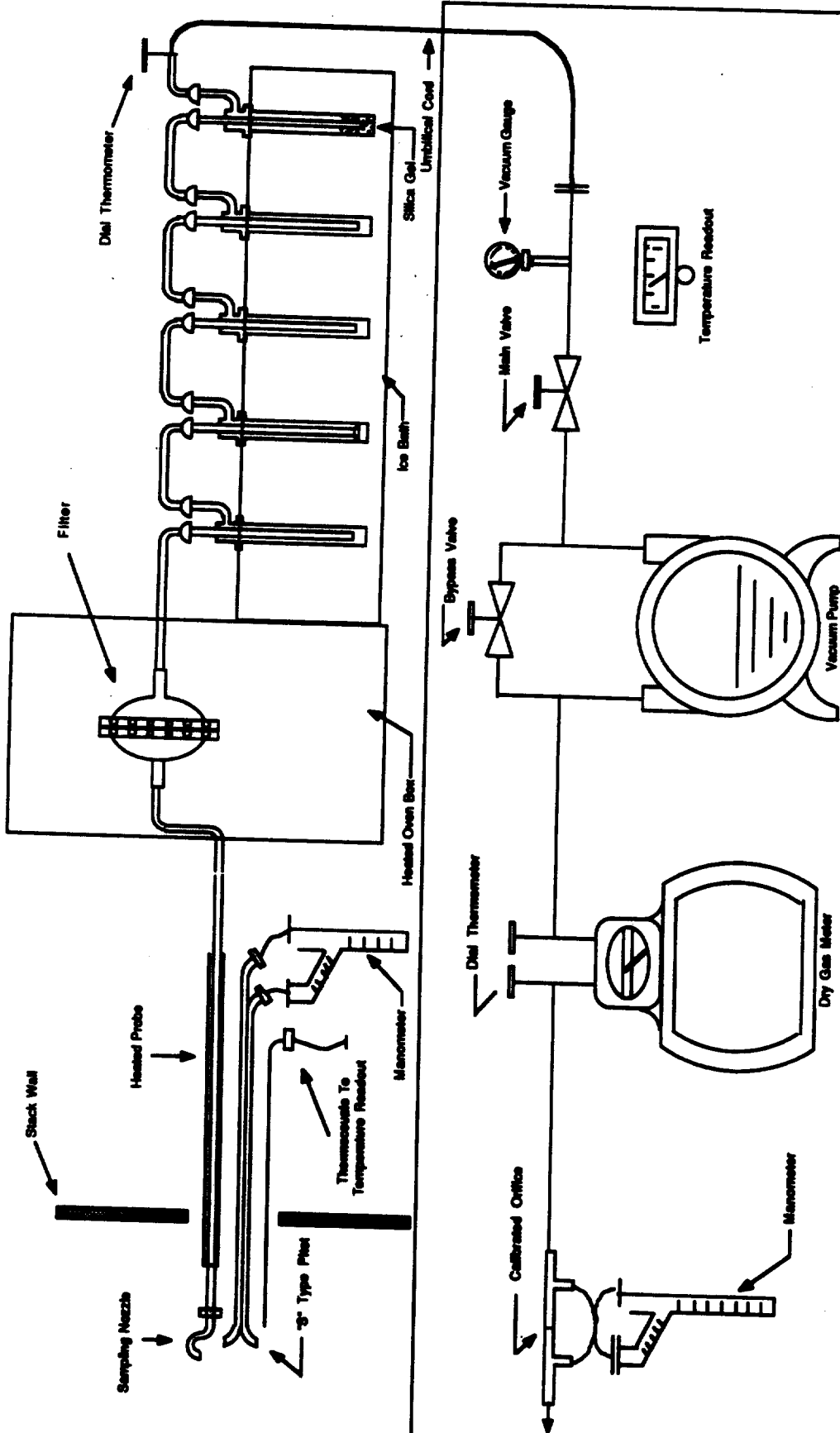
**SAMPLING AND ANALYTICAL METHODS:
DETERMINATION OF PARTICULATE AND METALS (11) EMISSIONS -
EPA MULTIPLE METALS METHOD (DRAFT: 8/28/89)**

In the laboratory, the acetone rinse sample (Container A) is poured into a pre-cleaned, pre-weighed beaker and evaporated to dryness. The filter (Container C) and beaker are then placed in a dessicator for conditioning, prior to weighing. After weighing, the filter is added to the beaker and the samples are digested; following digestion, the Container A/C, Container B, and Container D samples are concentrated and analyzed (separately) for each metal using the following instrumentation:

<u>Metal</u>	<u>Instrument</u>
Arsenic	Atomic Absorption (Graphite Furnace)
Beryllium	Inductively Coupled Plasma
Cadmium	Inductively Coupled Plasma
Chromium	Inductively Coupled Plasma
Copper	Inductively Coupled Plasma
Lead	Atomic Absorption (Graphite Furnace)
Manganese	Inductively Coupled Plasma
Mercury	Atomic Absorption (Cold Vapor)
Nickel	Inductively Coupled Plasma
Selenium	Atomic Absorption (Graphite Furnace)
Zinc	Inductively Coupled Plasma

The Container E sample (i.e., potassium permanganate/sulfuric acid solution) is first filtered and the filter is washed with permanganate. An aliquot of the filtrate is then analyzed for mercury (only) in accordance with CARB Method 101A (cold vapor atomic absorption), following the addition of potassium permanganate, nitric acid, and sodium chloride hydroxylamine.

The pre-weighed silica gel sample (Container F) is re-weighed and summed with the increase in impinger contents to determine the total volume of water condensed.



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Technical Services, Inc.
2116 Berkeley Way
Berkeley, CA 94704
Tel: (415) 848-0088
Fax: (415) 848-0038

SCALE: NA

DATE:

9/27/90

JOB NUMBER:

SE-034

DRAWN BY:

ML

CENTRAL CONTRA COSTA SANITARY DISTRICT

File:
Metals. Drwg

METALS SAMPLING TRAIN

Dist:
SE034

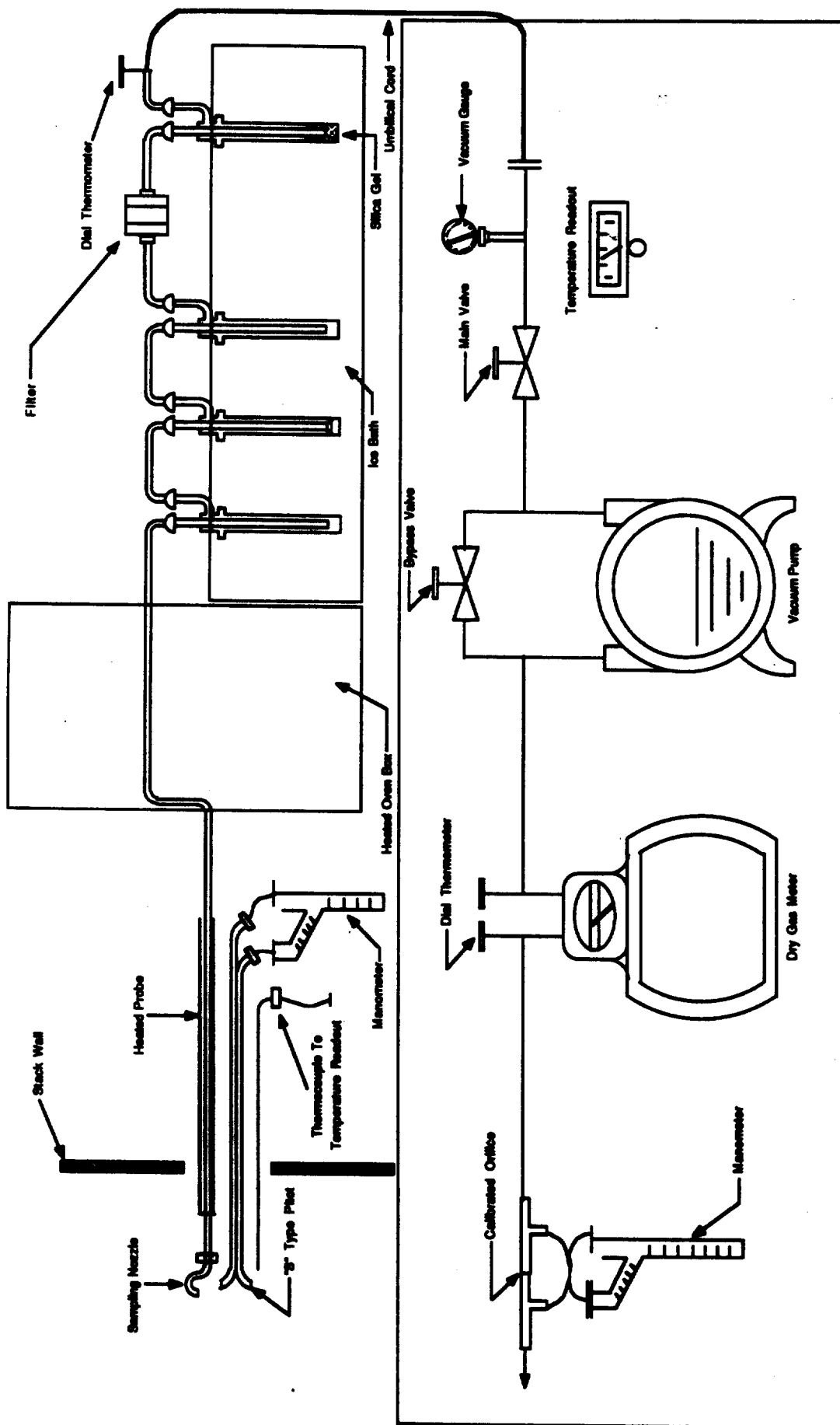
**SAMPLING AND ANALYTICAL METHODS:
HEXAVALENT CHROMIUM EMISSIONS - CARB METHOD 425**

Hexavalent chromium emission testing was performed in accordance with California Air Resources Board (CARB) Method 425 (amended, January 11, 1990). A schematic of the sampling train is presented on the following page. Velocity pressure of the stack gas is measured with a stausscheibe type pitot tube connected to an inclined gauge manometer. Isokinetic sampling rates are calculated using a nomograph and sample flow rate is regulated accordingly by adjusting the pressure drop across a calibrated orifice. Total sample volume is measured by a dry gas meter. Direct thermocouple read-out is provided for stack gas, impinger effluent, probe, sampling box, and the gas meter influent and effluent temperatures.

Stack gases are drawn through a glass nozzle, probe and oven assembly (non-heated) and bubbled through two impingers in series, each containing 100 milliliters of 0.1 N sodium hydroxide (NaOH) solution. Stack gases are then drawn through an empty impinger (for droplet/mist knockout) followed by an 85mm teflon-impregnated fiberglass filter (Pallflex Products #T60A20) meeting CARB specifications for removal efficiency. The sample gas then passes through a fourth impinger containing 300 grams of indicating silica gel, prior to entering the metering system.

Following the completion of sampling, the volume of the solution in the impingers is measured; the impinger contents and the rinse solution (0.1 N NaOH) are transferred to a storage container (Container #1). The filter is also removed and transferred to Container #1. The probe liner, sampling nozzle, filter holder, and connecting glassware are rinsed with 0.1 N NaOH, and the rinse is added to Container #1. The entire sampling train is then rinsed with 0.1 N nitric acid and the rinse is transferred to Container #2. Lastly, the silica gel in the fourth impinger is transferred to Container #3.

In the laboratory, the total volume of the Container #1 sample is measured. An aliquot of the sample is transferred to a beaker and acidified to a pH of approximately 1 (with 6 N sulfuric acid). After the addition of diphenylcarbazide (allowing approximately 10 minutes for color development), the sample is filtered and the absorbance is measured with a spectrophotometer at a wavelength of 540 nm. The absorbance of the sample is compared with solutions of known amounts to determine sample quantities. Field and laboratory (internal) blank samples are prepared and analyzed in conjunction with the samples to account for potential contamination and/or background levels. A second aliquot of the Container #1 solution is analyzed for total chromium using flame atomic absorption spectroscopy (AAS). The Container #2 solution is similarly analyzed for total chromium using AAS. The pre-weighed silica gel sample (Container #3) is re-weighed and summed with the increase in impinger contents to determine the total volume of water condensed.



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Technical Services, Inc.
2116 Berkeley Way
Berkeley, CA 94704
Tel: (415) 848-0366
Fax: (415) 848-0336

SCALE: NA

DATE: 9/7/90

JOB NUMBER: SE-034

DRAWN BY: ML

CENTRAL CONTRA COSTA SANITARY DISTRICT

HEXAVALENT CHROMIUM SAMPLING TRAIN (CARB METHOD 425)

File: Hex Chr. Drwg

Disk: SE034

**METHOD FOR THE DETERMINATION OF
POLYCHLORINATED DIBENZO-P-DIOXINS/DIBENZOFURANS
AND POLYCYCLIC AROMATIC HYDROCARBON EMISSIONS
(CARB METHODS 428 AND 429)**

Sampling and analysis for polychlorinated dibenzo-p-dioxins/dibenzofuran (PCDD/PCDF), and polycyclic aromatic hydrocarbon (PAH) emissions was performed in accordance with the California Air Resources Board (CARB) Methods 428 and 429. Stack gas samples were collected utilizing Modified Method 5 (MM5) procedures; a schematic of the train is shown on the following page. Velocity pressure of the stack gas is measured with an S-type pitot connected to an inclined gauge manometer. Isokinetic sampling rates are calculated using a nomograph, with sample flowrate regulated by adjusting the pressure drop across a calibrated orifice. Total sample volume is measured by a dry gas meter. Dial thermometers and/or thermocouples are employed to monitor stack gas, probe filter oven, XAD-2 trap effluent, impinger effluent and dry gas meter influent and effluent temperatures.

Stack gases are drawn isokinetically through a nozzle and heated borosilicate glass probe, and then through an 85 millimeter diameter glass fiber filter meeting CARB Method 5 specifications for particulate removal efficiency. Both probe and filter are maintained at $250 \pm 25^{\circ}\text{F}$ to avoid condensation. The sample gas is then drawn through teflon tubing and an ice water-cooled condenser/solid sorbent trap containing approximately 40 grams of XAD-2 resin. The resin trap is wrapped with aluminum foil (to avoid direct exposure to light) and the temperature of the sample gas is maintained below 68°F at the trap exit. Condensate percolates through the resin and is collected in a knock-out impinger; gases are then bubbled through a series of three impingers for additional moisture removal. The second and third impingers each contain 100 ml of deionized water and the fourth impinger contains approximately 300 grams of indicating silica gel; all impingers are pre-weighed on-site and placed in an ice bath to achieve a sample effluent temperature of less than 68°F .

Following the completion of sampling, the filter is removed and transferred to a storage bottle (Container #2). The probe liner, nozzle and all glassware preceding the filter are brushed and sequentially rinsed with methanol, benzene, and methylene chloride; the rinses are transferred to another storage bottle (Container #1). The teflon tubing, condenser, and glassware between the filter and resin trap are then rinsed with methanol, benzene, and methylene chloride; the rinses are transferred to a storage bottle (Container #3). The XAD-2 resin trap is next removed and sealed (Container #4). The impingers are then re-weighed to determine the quantity of moisture condensed; the contents of the knock-out impinger are transferred to a storage container (Container #5) along with the methanol, benzene, and methylene chloride rinse of the impinger. The contents of the second and third impinger are transferred to a storage bottle (Container #6).

**METHOD FOR THE DETERMINATION OF
POLYCHLORINATED DIBENZO-P-DIOXINS/DIBENZOFURANS
AND POLYCYCLIC AROMATIC HYDROCARBON EMISSIONS
(CARR METHODS 428 AND 429)**

along with a deionized water rinse of these impingers and all connecting glassware. Lastly, the silica gel in the final impinger is transferred to a storage bottle (Container #7), completing the sample recovery process.

Special precautions are taken to avoid sample contamination. All sampling train components upstream of the silica gel impinger are pre-cleaned in accordance with EPA's Manual of Analytical Methods for the Analysis of Pesticide Residues in Human and Environmental Samples, with special attention paid to removing silicon grease from the glassware joints. All glassware was then rinsed with methylene chloride prior to use. No grease is utilized in the sampling train and all gaskets coming in contact with the sample are teflon. Also, sample recovery is performed in a clean area away from the emission source (and other potential sources of contamination) being tested; all (pre-cleaned) sample storage containers have teflon-lined caps. Sampling reagents (filters and XAD-2 resin) are pre-cleaned via soxhlet extraction and spiked with surrogate standard compounds. Lastly, a blank train is assembled and recovered in the field; the blank train is analyzed in conjunction with the samples to document whether contamination occurred.

Sample containers 1-6 are analyzed for PCDD/PCDF and PAH compounds utilizing high resolution gas chromatography/mass spectrometry (HRGC/MS). The following homologue groups and isomers are quantified.

PCDD/PCDF:

2,3,7,8 TCDD
Total TCDD
1,2,3,7,8 PeCDD
Total PeCDD
1,2,3,4,7,8 HxCDD
1,2,3,6,7,8 HxCDD
1,2,3,7,8,9 HxCDD
Total HxCDD
1,2,3,4,6,7,8 HpCDD
Total HpCDD
Total OCDD

2,3,7,8 TCDF
Total TCDF
1,2,3,7,8 PeCDF
2,3,4,7,8 PeCDF
Total PeCDF
1,2,3,4,7,8 HxCDF
1,2,3,6,7,8 HxCDF
2,3,4,6,7,8 HxCDF
1,2,3,7,8,9 HxCDF
Total HxCDF
1,2,3,4,6,7,8 HpCDF
1,2,3,4,7,8,9 HpCDF
Total HpCDF
Total OCDF

**METHOD FOR THE DETERMINATION OF
POLYCHLORINATED DIBENZO-P-DIOXINS/DIBENZOFURANS
AND POLYCYCLIC AROMATIC HYDROCARBON EMISSIONS
(CARB METHODS 428 AND 429)**

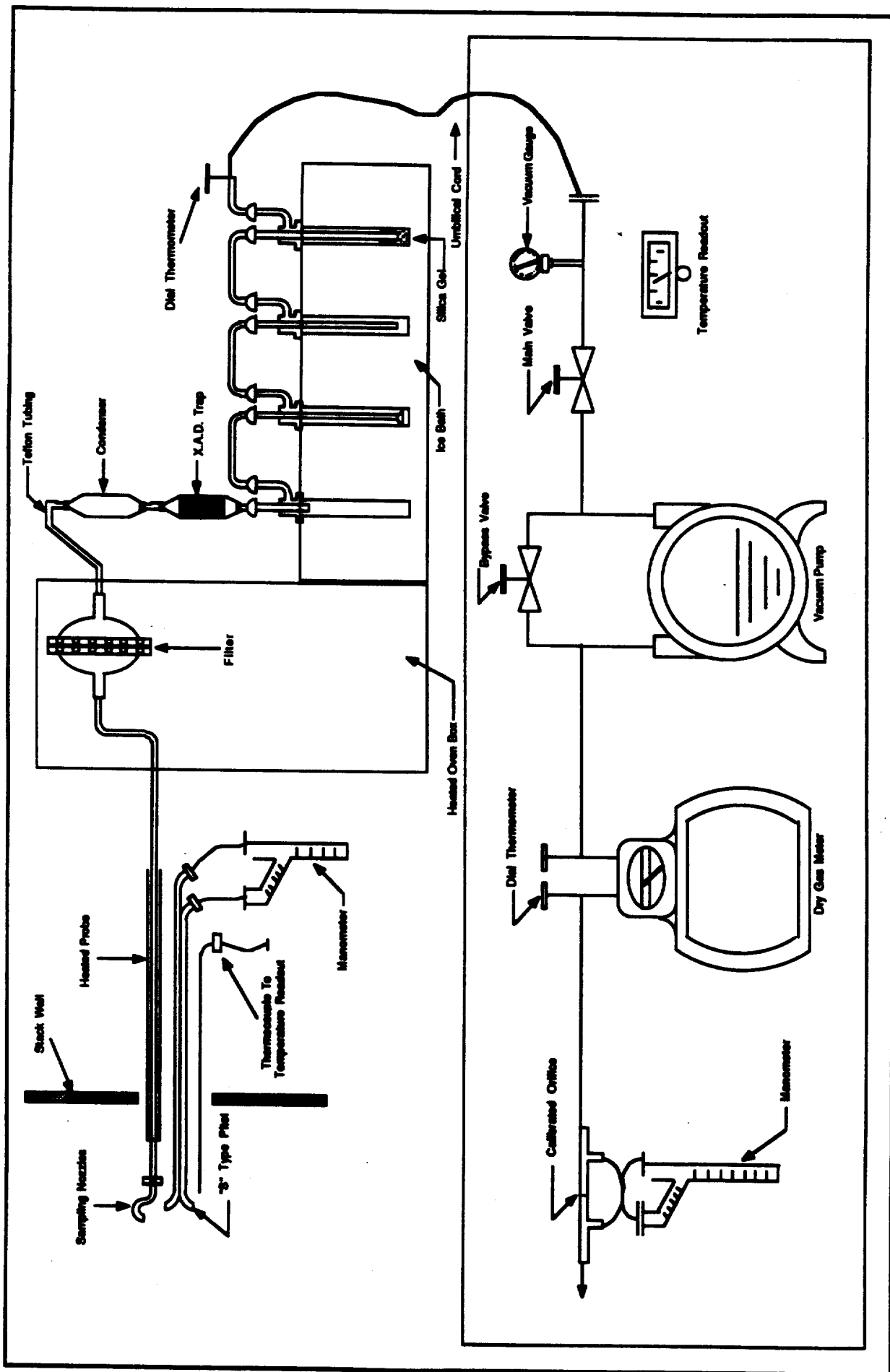
PAH Compounds:

Naphthalene	2-Methylnaphthalene
2-Chloronaphthalene	Acenaphthylene
Acenaphthene	Fluorene
Phenanthrene	Anthracene
Fluoranthene	Benzo(a)anthracene
Chrysene	Benzo(b)fluoranthene
Benzo(k)fluoranthene	Benzo(a)pyrene
Perylene	Indeno(1,2,3-cd)pyrene
Dibenz(a,h)anthracene	Benzo(g,h,i)perylene

The silica gel sample (Container 7) was re-weighed and summed with the increase in impinger contents to determine the total volume of water condensed.

In the laboratory, the samples and/or extracts corresponding to Containers 1-6 are combined and prepared for analysis in accordance with CARB Method 428 procedures. All samples (including the blanks) are fortified with internal and surrogate standards prior to preparation. Following sample clean-up steps, the final residue is dissolved in 20 μ l of toluene, containing carbon-labeled internal standards used for determining recovery efficiencies. The sample was then split; half of the solution was utilized for the PCDD/PCDF analysis, while the other half was used for the PAH analyses. The instruments and conditions utilized to perform the analyses are summarized on the following pages.

Prior to sample analyses, the mass spectrometer response was initially calibrated with several standard solutions containing known amounts of the PCDD/PCDF and PAH isomers of interest. In addition, a continuing calibration was demonstrated every 12 hours using one of the solutions. Response factors used for the calculation of the analyte concentrations were obtained from the daily continuing calibration checks.



GALSON Technical Services, Inc. 2118 Berkeley Way Berkeley, CA 94704 Tel: (415) 848-0369 Fax: (415) 848-0338	SCALE: NA DATE: 5/11/90	JOB NUMBER: SE-034	CENTRAL CONTRA COSTA SANITARY DISTRICT	File: PAH. Drwg
		DRAWN BY: MSL	PCDD/PCDF AND PAH SAMPLING TRAIN (CARB METHOD 429)	Disk: SE034

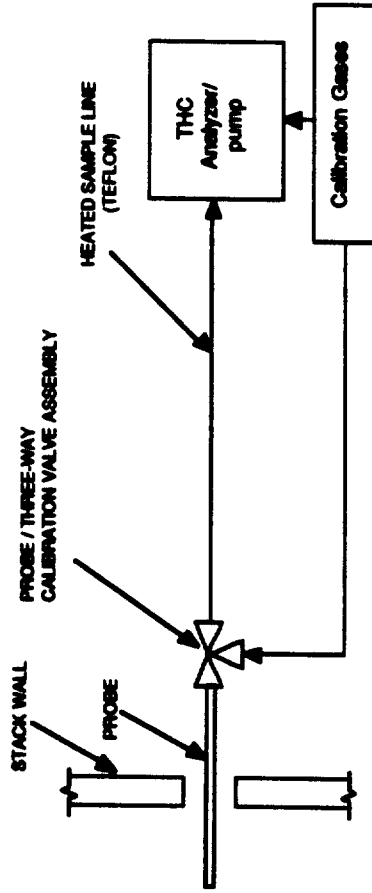
**SAMPLING AND ANALYTICAL METHODS:
TOTAL HYDROCARBON EMISSIONS - EPA METHOD 25A
(CONTINUOUS MONITORING PROCEDURE)**

Stack gas concentrations of total gaseous hydrocarbons (THC) were determined in accordance with the Environmental Protection Agency Method 25A. A Ratfish Instruments, Ltd. (Model RS 55) THC analyzer was utilized to perform the testing. Data were recorded using a Linear Instruments strip chart recorder. A schematic of the sampling train is shown on the following page.

Stack gases are drawn through the probe and heated sampling line to the analyzer. The instrument is equipped with an integral heated filter/leak-free diaphragm pump and a flame ionization detector (FID). The sampling rate of the analyzer is approximately 4 l/min. The FID is fueled with high purity hydrogen; hydrocarbon-free combustion air is also supplied to the analyzer. All materials in contact with the sample gas stream are either teflon or stainless steel.

Instrument outputs include an analog signal display and 0 to 1 volt recorder terminals; full scale responses are selectable in four ranges corresponding to THC concentrations spanning from 0-10 ppm to 0-500 ppm. The strip chart recorder is connected to the recorder terminals and continuously records the instantaneous output from the analyzer; subsequent data reduction includes converting voltage outputs to THC concentrations (based on instrument calibration) and averaging the concentration data for the time period of interest. Total hydrocarbons are measured on a wet basis, as methane; concentrations are corrected to dry conditions using the moisture content of the stack gas.

Instrument calibration is performed on-site utilizing zero air and methane (in air) certified gas standards. Prior to the start of testing, the instrument is calibrated directly by introducing each calibration gas directly to the instrument; a system bias check is then performed by introducing each gas at the probe/three-way valve assembly. The calibration check is repeated at the conclusion of the testing; acceptable performance specifications include a zero/calibration drift of up to $\pm 3\%$.



GALSON Technical Services, Inc. 2118 Berkeley Way Berkeley, CA 94704 Tel: (415) 848-0350 Fax: (415) 848-0838	SCALE: NA DATE: 9/27/90	JOB NUMBER: SE-034	CENTRAL CONTRA COSTA SANITARY DISTRICT THC SAMPLING SYSTEM	File: THC. Dwg
		DRAWN BY: ML		Disk: SE034

**SAMPLING AND ANALYTICAL METHODS:
CARBON MONOXIDE - EPA METHOD 10
(CONTINUOUS MONITORING PROCEDURE)**

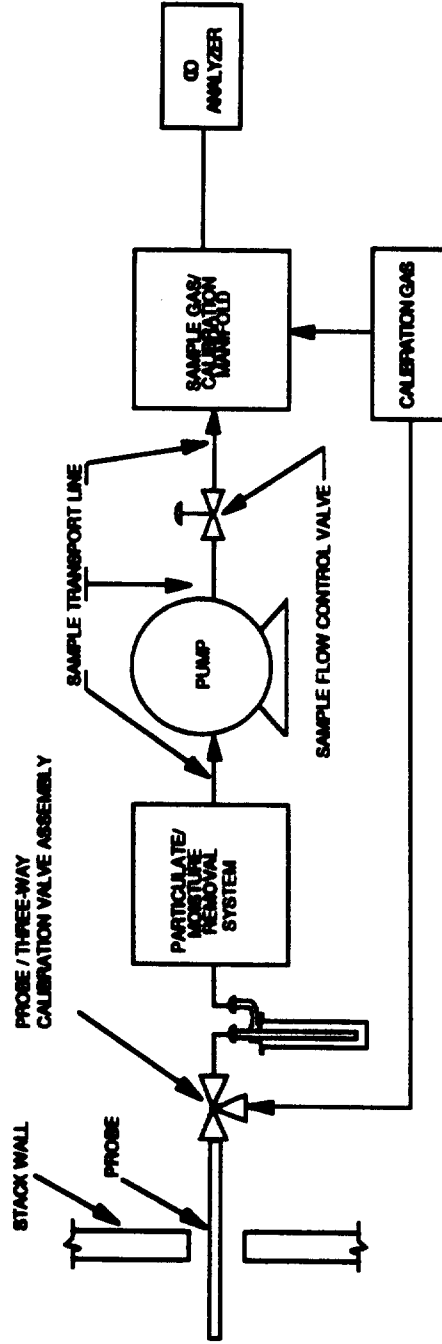
Stack gas concentrations of carbon monoxide were determined in accordance with the Environmental Protection Agency (EPA) Method 10. A gas correlation non-dispersive infrared analyzer manufactured by Thermo Electron Corporation (TECO Model 48) was utilized to perform the testing. The stack gas conditioning system consisted of a glass wool filter and a condenser/knock-out impinger for particulate and moisture removal. Data were recorded using a Linear Instruments strip chart recorder. A schematic of the sampling train is shown on the following page.

Stack gases are drawn through the probe/filter assembly and three-way valve, followed by the condenser/knock-out impinger. The sample gas then passes through teflon tubing and into the analyzer which is equipped with a leak-free diaphragm pump; the sampling rate of the analyzer is approximately 1 l/min. All materials in contact with the sample gas stream are either teflon or stainless steel.

The TECO analyzer determines CO concentrations by measuring the absorbance of the sample in the infrared region. Gas filter correlation is employed to improve the specificity and sensitivity of the method. Instrument outputs include a digital readout and 0-1V recorder terminals; full scale responses are selectable in ten ranges corresponding to CO concentrations spanning from 0-1 ppm to 0-1,000 ppm. The strip chart recorder is connected to the recorder terminals and continuously records the instantaneous output from the analyzer; subsequent data reduction includes converting voltage outputs (i.e., chart recorder units) to CO concentrations (based on instrument calibration) and averaging concentrations for the time period of interest.

The instrument is periodically checked for interference from SO₂, NO_x, and CO₂, with a maximum response of 2% of full scale considered acceptable. Other gases are checked on a case-by-case basis if they are expected to be present and/or potential interferences.

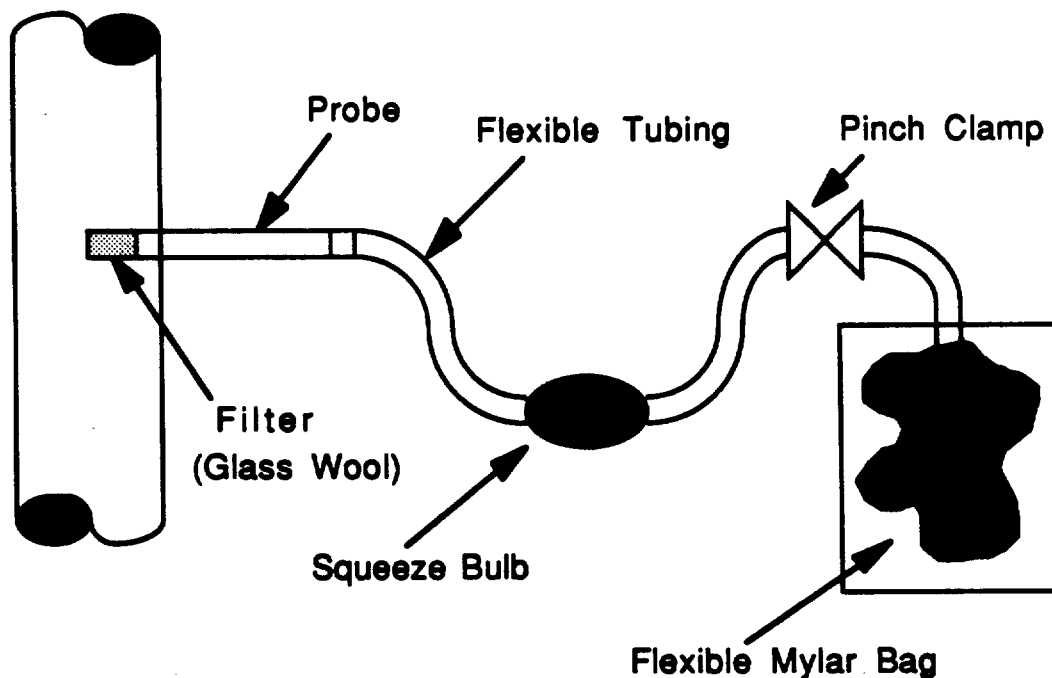
Instrument calibration is performed on-site utilizing zero air and a CO in nitrogen certified gas standard. Prior to the start of testing, the instrument is calibrated directly by introducing each calibration gas to the sample gas manifold; a system bias check is then performed by introducing each gas at the probe/three-way valve assembly. The calibration check is repeated at the conclusion of the testing; acceptable performance specifications include a zero/calibration drift of up to $\pm 3\%$.



GALSON Technical Services, Inc. 2118 Barbary Way Berkeley, CA 94704 Tel: (415) 848-0389 Fax: (415) 848-0338	SCALE: NA	JOB NUMBER: SE-034	CENTRAL CONTRA COSTA SANITARY DISTRICT	File: CO. Dwg Diet: SE034
	DATE: 5/14/90	DRAWN BY: MSL	CO SAMPLING SYSTEM	

**SAMPLING AND ANALYTICAL METHODS: CO₂, O₂, AND
CO CONCENTRATIONS (PERCENT LEVELS)
(CARB METHOD 3)**

Stack gas concentrations of CO₂, O₂, and CO (percent levels) were determined in accordance with California Air Resources Board (CARB) Method 3. An integrated gas sample was collected utilizing the sampling train shown below. After evacuating the sampling bag, gas sample was drawn from the exhaust stack using a squeeze bulb. Multiple point sampling was performed and an equal volume of sample was collected at each point. A total sample volume of approximately 20 liters was collected during the sampling interval. Samples were analyzed for CO₂, O₂, and CO (percent levels) utilizing an Orsat apparatus; each sample was analyzed in duplicate (at minimum). Results are reported to the nearest 0.1 percent.



Galson

Technical Services, Inc.
2116 Berkeley Way
Berkeley, CA 94704
Tel: (415) 848-0389
Fax: (415) 848-0838

SCALE:
N/A

JOB NUMBER:
SE-034

CO₂ AND O₂ ANALYSIS

File:
CARB M3. Drwg

DATE:
9/7/90

DRAWN:
ML

CARB METHOD 3

Disk:
SE034

APPENDIX IV: CALIBRATION DATA

PRE-TEST CALIBRATION DATA

Technical Services, Inc.
2110 Berkeley Way
Berkeley, CA 94704
Tel: (415) 848-0300
Fax: (415) 848-0630

Orifice and Dry Test Meters

Date 4/9/90
Meter Box ID 004
Wet Test Meter ID GTS#2
Barometric Pressure 30.14

ORIFICE READING (ΔH_0) in H_2O	WET TEST METER		DRY GAS METER						δ	ΔH_a			
	GAS VOLUME (V_w) l ³	TEMP. (T_w) °F	GAS VOLUME (V_g) l ³	TEMPERATURE DATA °F			$T_{D\text{ avg}}$						
				Time	$T_{D\text{ in}}$	$T_{D\text{ out}}$							
0.56	3.0	66 (526)	933.745 930.87 30.78				86 88 90	78 78 78	83 (543)	7:35.52 (7.542)	1.005	1.92	
1.0	4.0	66 (526)	938.064 933.945 4.119				96 99 103	79 80 81	89.7 (549.7)	7:20.02 (7.334)	1.012	1.78	
2.0	6.0	66 (526)	944.295 938.064 6.231				108 113 115	82 84 85	97.8 (557.8)	8:03.22 (8.066)	1.016	1.89	
4.0	8.0	66 (526)	952.646 944.295 8.351				119 123 125	88 91 91	106.2 (566.2)	7:38.22 (7.645)	1.021	1.88	
											Average	1.014	1.87

$$\delta = \frac{V_w}{V_g} \left(\frac{T_{D\text{ avg}} + 460}{T_w + 460} \right) \cdot \frac{P_b}{\left(P_b + \frac{\Delta H_0}{13.6} \right)}$$

Technician: DR

$$\delta = \frac{V_w}{V_D} \left(\frac{T_{D,avg} + 460}{T_w + 460} \right) \frac{P_b}{(P_b + \frac{\Delta H_b}{13.6})}$$

$$\Delta H_o = 0.0317 \Delta H_o \left(\frac{1}{V_w} \right)^2 \frac{(T_w + 460)^2}{P_b (T_o + 460)}$$

Galson

Technical Services, Inc.
2119 Berkeley Way
Berkeley, CA 94704
Tel: (415) 848-0380
Fax: (415) 848-0338

Calibration Data - Stack Sampling Train

Orifice and Dry Test Meters

Date 4-3-90 Wet Test Meter ID GTS#2

Meter Box ID 005 Barometric Pressure 30.26

WET TEST METER		DRY GAS METER					TIME Δt min.	δ	ΔH_0
ORIFICE READING (ΔH_0) in. H_2O	GAS VOLUME (V_w) ft ³	TEMP. (T_w) °F	GAS VOLUME (V_0) ft ³	TEMPERATURE DATA °F					
				Time	$T_{0\text{ in}}$	$T_{0\text{ out}}$	$T_{0\text{ avg}}$		
0.5	3.0	68	18.043 <u>14.972</u> 3.071		80 84 86	78 79 79	81.0 (7:21.69) 7.36	1.000	1.62
1.0	4.0	68	23.128 <u>19.000</u> 4.128		90 93 95	82 83 84	87.8 (7:06.62) 7.11	1.004	1.68
2.0	6.0	68	30.011 <u>23.803</u>		99 102 104	86 88 89	94.7 (7:44.09) 7.73	1.010	1.75
4.0	8.0	68	40.326 <u>32.000</u> 8.326		106 109 111	91 92 94	100.5 (7:28.08) 7.47	1.011	1.82
								Average	1.006
									1.72

$$\delta = \frac{V_w}{V_0} \left(\frac{T_{0\text{ avg}} + 460}{T_w + 460} \right) \frac{P_0}{P_1} \frac{\Delta H_0}{\Delta H_1}$$

Technician: R. RAMER

Technician: R. RAMER

$$\delta = \frac{V_w}{V_0} \left(\frac{T_{0\text{avg}} + 460}{T_w + 460} \right) \frac{P_0}{P_0 + \frac{\Delta H_0}{13.6}}$$

$$\Delta H_0 = 0.0317 \Delta H_0 \left(\frac{1}{V_w} \right)^2 \frac{(T_w + 460)^2}{P_0 (T_0 + 460)}$$

Thermocouple Calibration Data

Type: M-5-I (DIAL)
M-5-O (DIAL)

ICE WATER BATH	
	Temp. °R
Standard	492
M-5-I	493
% Deviation	0.2
Standard	492
M-5-O	497
% Deviation	1.0
Standard	
% Deviation	

AMBIENT	
	Temp. °R
Standard	532
M-5-I	532
% Deviation	0.0
Standard	532
M-5-O	537
% Deviation	0.9
Standard	
% Deviation	

HOT WATER BATH	
	Temp. °R
Standard	672
M-5-I	668
% Deviation	0.6
Standard	672
M-5-O	669
% Deviation	0.4
Standard	
% Deviation	

Date: 7/6/89
 Technician: [Signature]

Thermocouple Calibration Data

Type: K (stack)

ICE WATER BATH	
	Temp. °R
Standard <u>T-7 (4')</u>	492
% Deviation	492
Standard <u>T-8 (8')</u>	492
% Deviation	492
Standard	
% Deviation	

AMBIENT	
	Temp. °R
Standard <u>T-7</u>	524
% Deviation	523
Standard <u>T-8</u>	524
% Deviation	523
Standard	
% Deviation	

HOT WATER BATH	
	Temp. °R
Standard <u>T-7</u>	672
% Deviation	672
Standard <u>T-8</u>	672
% Deviation	672
Standard	
% Deviation	

Date: 2/6/90

Technician: D. Roberts

Thermocouple Calibration Data

Type: Stack Thermocouples

ICE WATER BATH	
	Temp. °R
Standard	495
T-1	492
% Deviation	0.6
Standard	495
T-2	492
% Deviation	0.6
Standard	495
T-3	492
% Deviation	0.6

AMBIENT	
	Temp. °R
Standard	532
T-1	532
% Deviation	0.0
Standard	532
T-2	533
% Deviation	0.2
Standard	532
T-3	532
% Deviation	0.0

HOT WATER BATH	
	Temp. °R
Standard	672
T-1	671
% Deviation	0.1
Standard	672
T-2	670
% Deviation	0.3
Standard	672
T-3	671
% Deviation	0.1

Date: 7 July '89

Technician: AR

Thermocouple Calibration Data

Type: Oven box

ICE WATER BATH	
	Temp. °R
Standard	492
OB-2	494
% Deviation	0.40
Standard	
% Deviation	
Standard	
% Deviation	

AMBIENT	
	Temp. °R
Standard	531
OB-2	527
% Deviation	0.75
Standard	
% Deviation	
Standard	
% Deviation	

HOT WATER BATH ^{OVEN}	
	Temp. °R
Standard	687
OB-2	688
% Deviation	0.15
Standard	
% Deviation	
Standard	
% Deviation	

Date: 10/17/89

Technician: D. Roberts

Thermocouple Calibration Data

Type: Oven Box Thermocouple

ICE WATER BATH	
	Temp. °R
Standard	492
OB-1	492
% Deviation	0.00
Standard	
% Deviation	
Standard	
% Deviation	

AMBIENT	
	Temp. °R
Standard	5.27
OB-1	5.25
% Deviation	0.38
Standard	
% Deviation	
Standard	
% Deviation	

HOT WATER BATH	
	Temp. °R
Standard	722
OB-1	721
% Deviation	0.14
Standard	
% Deviation	
Standard	
% Deviation	

Date: 9/12/89

Technician: D. Roberts

Thermocouple Calibration Data

Type: Impinger

ICE WATER BATH	
	Temp. °R
Standard	492
I-2	492
% Deviation	0.00
Standard	
% Deviation	
Standard	
% Deviation	

AMBIENT	
	Temp. °R
Standard	528
I-2	528
% Deviation	0.00
Standard	
% Deviation	
Standard	
% Deviation	

HOT WATER BATH	
	Temp. °R
Standard	672
I-2	668
% Deviation	0.60
Standard	
% Deviation	
Standard	
% Deviation	

Date: 9/12/89

Technician: V. Rollett

THERMOCOUPLE TEMPERATURE CALIBRATION

ICE WATER BATH	
	Temp. °R
Standard	49.2
Thermocouple I-4	49.3
% Deviation	0.20
Standard	
Thermocouple	
% Deviation	
Standard	
Thermocouple	
% Deviation	

AMBIENT	
	Temp. °F
Standard	53.1
Thermocouple I-4	52.9
% Deviation	0.38
Standard	
Thermocouple	
% Deviation	
Standard	
Thermocouple	
% Deviation	

HOT WATER BATH	
	Temp. °R
Standard	68.8
Thermocouple I-4	68.5
% Deviation	0.44
Standard	
Thermocouple	
% Deviation	
Standard	
Thermocouple	
% Deviation	

Date: 10/17/89

Technician: W. Phert

Thermocouple Calibration Data

Type: XAD TYPE

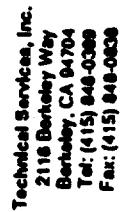
ICE WATER BATH	
	Temp. °R
Standard	492
P-3	492
% Deviation	0.09%
Standard	
% Deviation	
Standard	
% Deviation	

AMBIENT	
	Temp. °R
Standard	528
P-3	527
% Deviation	0.19%
Standard	
% Deviation	
Standard	
% Deviation	

HOT WATER BATH	
	Temp. °R
Standard	672
P-3	671
% Deviation	0.15%
Standard	
% Deviation	
Standard	
% Deviation	

Date: 7/23/90

Technician: T.Z.



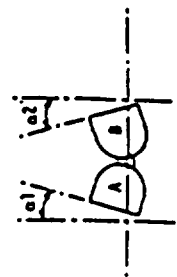
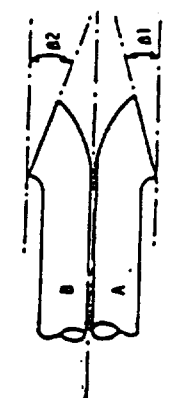
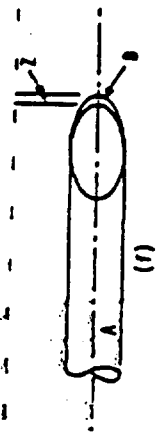
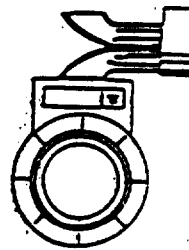
68/E/11

Date: 11/7/89

1. D_I - external tubing diameter
 $0.188'' < D_I < 0.375''$
 $D_I = \underline{0.371}$ inches
2. $P = (P_a + P_b)/2$
 $1.05 D_I < P < 1.50 D_I$
 $P_a + P_b = \underline{1.034}$ inches
 $P = \underline{0.517}$ inches
3. $Z = (P_a + P_b) \sin \gamma$
 $Z < 0.125''$
 $\gamma = \underline{1}$ inches
 $Z = \underline{0.018}$ inches
4. $W = (P_a + P_b) \sin \sigma$
 $W < 0.031''$
 $\sigma = \underline{1}$ inches
 $W = \underline{0.018}$ inches
5. $\beta_A, \beta_B < 5^\circ$
 $\beta_A = \underline{1}$
 $\beta_B = \underline{1}$
6. $\alpha_A, \alpha_B < 10^\circ$
 $\alpha_A = \underline{2}$
 $\alpha_B = \underline{1}$

*Acceptable limits; "Standards of Performance for New Stationary Sources," Federal Register, 36 (247), December 23, 1971.

***Acceptable limits; Vollaro, R. F., "The Effects of Impact Opening Misalignment on the Value of the Type-S Pilot Tube Coefficient", U.S. EPA Emission Measurement Branch, Research Triangle Park, NC, October 1976



Terrill, T. A. A.

Galson

Technical Services, Inc.
2116 Berkeley Way
Berkeley, CA 94704
Tel: (415) 848-0360
Fax: (415) 848-0838

PITOT TUBE CALIBRATION

VERIFICATION OF CONSTRUCTION SPECIFICATIONS

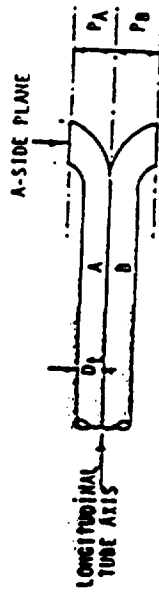
Pilot ID: P-1 (2')

Date: 11/14/84

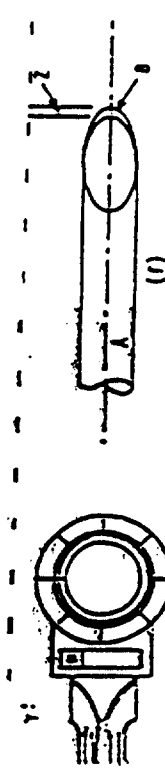
1. D_I - external tubing diameter
 $0.180" < D_I < 0.375"$ inches
 $D_I = \underline{0.370}$ inches
2. $P = (P_A + P_B)/2$ inches
 $P_A + P_B = \underline{1.018}$ inches
 $P = \underline{0.509}$ inches
3. $Z = (P_A + P_B) \sin \gamma$ inches
 $Z < 0.125"$..
 $\gamma = \underline{1^\circ}$
 $Z = \underline{0.018}$ inches
4. $W = (P_A + P_B) \sin \sigma$ inches
 $W < 0.031"$..
 $\sigma = \underline{1.5^\circ}$
 $W = \underline{0.027}$ inches
5. $\beta_A, \beta_B < 5^\circ$..
 $\beta_A = \underline{0^\circ}$
 $\beta_B = \underline{1^\circ}$
6. $\alpha_A, \alpha_B < 10^\circ$..
 $\alpha_A = \underline{15^\circ}$
 $\alpha_B = \underline{3.5^\circ}$

*Acceptable limits: "Standards of Performance for New Stationary Sources," Federal Register, 36 (247), December 23, 1971.

**Acceptable limits: Vollaro, R. F., "The Effects of Impact Opening Misalignment on the Value of the Type-S Pitot Tube Coefficient", U.S. EPA Emission Measurement Branch, Research Triangle Park, NO, October 1976



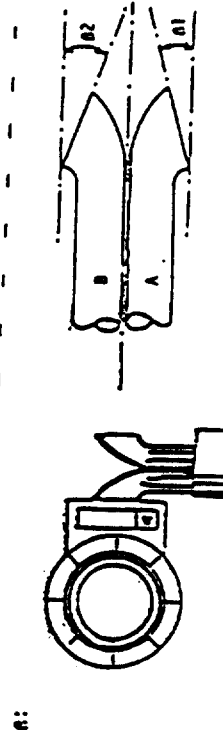
A-SIDE PLANE



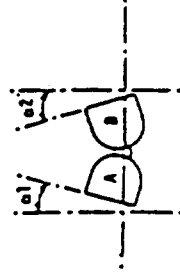
(1)



(2)



(3)



Technician: A. P. Pelt

POST-TEST CALIBRATION DATA

Galson

Technical Services, Inc.
2116 Berkeley Way
Berkeley, CA 94704
Tel: (415) 848-0399

POST TEST CALIBRATION - DRY GAS METER

Plant CCCSO-AB2588

Job # SE-034

Source Unit 2 - Stack

Meter Box ID 004

Barometric Pressure, in Hg 29.94

Date 5/7/90

ORIFICE READING (ΔH_0) in. H ₂ O	WET TEST METER		DRY GAS METER				TIME Δt min.	γ	ΔH_0	
	GAS VOLUME (V _w) l ₃	TEMP. (T _w) °F	GAS VOLUME (V ₀) l ₃	TEMPERATURE DATA °F						
				Time	T _{0 in}	T _{0 out}				T _{0 avg}
2.4	7.01	70 (530)	266.417		81	75	84.5	8:40.71	1.001	2.02
			259.267		91	76				
			7.150		93	73	(544.5)	8.679		
2.4	7.0	70 (530)	273.624		100	82	92.3	8:42.22	1.006	2.00
			266.417		102	82				
			7.207		106	82	(552.3)	8.704		
2.4	7.0	70 (530)	280.898		98	84	95.3	8:44.65	1.002	2.01
			273.624		106	85				
			7.274		112	87	(555.3)	8.744		
AVERAGE								1.003	2.01	
PRE-TEST γ								1.014	1.87	

$$\gamma = \frac{V_w}{V_0} \left(\frac{T_0 \text{ avg} + 460}{T_w + 460} \right) \left(\frac{P_0}{P_0 + \frac{\Delta H_0}{13.6}} \right)$$

Vacuum Setting. 5 in. Hg.

$$\gamma = \frac{V_w}{V_D} \left(\frac{T_D \text{ avg} + 460}{T_w + 460} \right) \frac{P_b}{(P_b + \frac{\Delta H_0}{13.6})}$$

Vacuum
Setting,
in. Hg.

5

$$\Delta H_0 = 0.0317 \Delta H_D \left(\frac{1}{V_w} \right)^2 \frac{(T_w + 460)^2}{P_b (T_D + 460)}$$

POST TEST CALIBRATION - TEMPERATURE SENSORS

	Ambient (°R)	% Diff.	Other (°R)	% Diff.
Reference	<u>529</u>	<u>0.2%</u>	<u>671</u>	<u>0</u>
Stack Thermocouple ID# <u>T-2</u>	<u>530</u>		<u>671</u>	
Reference	<u>533</u>	<u>0.2%</u>	<u>671</u>	<u>0.1%</u>
Gas Meter Inlet ID# <u>M-4-I</u>	<u>532</u>		<u>669</u>	
Reference	<u>533</u>	<u>0.8%</u>	<u>492</u>	<u>0.8%</u>
Gas Meter Outlet ID# <u>M-4-O</u>	<u>537</u>		<u>496</u>	
Reference	<u>532</u>	<u>0</u>	<u>670</u>	<u>0.4%</u>
Condenser Outlet ID# <u>T-2</u>	<u>532</u>		<u>667</u>	
Reference	<u>529</u>	<u>0.2%</u>	<u>702</u>	<u>0.1%</u>
Heated Oven Box ID# <u>OB-2</u>	<u>527</u>		<u>701</u>	
Technician: <u>Chris Tappan</u>		Date: <u>5-7-90</u>		

N/A - Not Applicable

Galson

Technical Services, Inc.
2118 Berkeley Way
Berkeley, CA 94704
Tel (415) 848-0389

POST TEST CALIBRATION - DRY GAS METER

Plant CLLSP-AB2588
Source Unit 2 Stack
Barometric Pressure, in Hg 29.97

Job # 56-034
Meter Box ID 005
Date 5-8-90

ORIFICE READING (ΔH_0) in. H ₂ O	WET TEST METER		DRY GAS METER				TIME Δt min.	γ	ΔH_0	
	GAS VOLUME (V _w) ft ³	TEMP. (T _w) °F	GAS VOLUME (V ₀) ft ³	TEMPERATURE DATA °F						
				Time	T _{0 in}	T _{0 out}				T _{0 avg}
1.8	6.05	71 (531)	452.376		91	89	93- (553)	8:00.78 (8.013)	1.002	1.70
			452.113		96	90				
			6.263		102	90				
1.8	6.0	70 (530)	430.968		86	80	92.67 (552.57)	7:52.36 (7.973)	1.018	1.71
			432.25		100	82				
			6.113		104	89				
1.8	6.0	70 (530)	446.025		98	89	94.5 (554.5)	7:59.86 (7.998)	1.007	1.72
			439.259		100	88				
			6.206		105	89				

$$\gamma = \frac{V_w}{V_0} \left(\frac{T_0 \text{ avg} + 460}{T_w + 460} \right) \left(\frac{P_0}{P_0 + \frac{\Delta H_0}{13.6}} \right) = 1.324$$

Vacuum
Setting.
in. Hg.

6.0-7.0

AVERAGE

1.009

1.71

PRE-TEST
 γ

1.006

1.72

$$\Delta H_0 = 0.0317 \Delta H_0 \left(\frac{1}{V_w} \right)^2 \frac{(T_w + 460)^2}{P_0 (T_0 + 460)}$$

(4-3-90)

POST TEST CALIBRATION - TEMPERATURE SENSORS				
	Ambient (°R)	% Diff.	Other (°R)	% Diff.
Reference	<u>530</u>	<u>0.2%</u>	<u>669</u>	<u>0.1%</u>
Stack Thermocouple ID# <u>I-7</u>	<u>529</u>		<u>668</u>	
Reference	<u>530</u>	<u>0</u>	<u>671</u>	<u>0</u>
Gas Meter Inlet ID# <u>M-5-I</u>	<u>530</u>		<u>671</u>	
Reference	<u>530</u>	<u>1.1%</u>	<u>669</u>	<u>0.7%</u>
Gas Meter Outlet ID# <u>M-5-O</u>	<u>536</u>		<u>674</u>	
Reference	<u>530</u>	<u>0.8%</u>	<u>494</u>	<u>0</u>
Condenser Outlet ID# <u>I-4</u>	<u>526</u>		<u>494</u>	
Reference	<u>534</u>	<u>0</u>	<u>694</u>	<u>0</u>
Heated Oven Box ID# <u>OB-1</u>	<u>534</u>		<u>694</u>	
Technician: <u>Clair Tandy</u>		Date: <u>5-8-90</u>		

ATA - Not Applicable

ON-SITE MONITOR CALIBRATION DATA



Galson
-Technical Services

Comments:

PRE-TEST & POST-TEST SYSTEM DRIFT CHECKS

Plant I. D. CCSO Project No. SE-034
Source Incinerator #2 Operator MR
Pollutant CO Analyzer I. D. TECO-48

Run No. 1

Date/Time 4/10/90 - 1138-1245

	Analyzer Calibration Response	Initial values		Final values		
		System Calibration Response	System bias (% of span)	System Calibration Response	System bias	Drift
					(% of span)	
Zero gas	0.0	0.0	0.0	0.0	0.0	0.0
Mid-range	450	450	0.0	445	1.0	1.0

Run No. 2

Date/Time 4/10/90 - 1357-1505

	Analyzer Calibration Response	Initial values		Final values		
		System Calibration Response	System bias (% of span)	System Calibration Response	System bias	Drift
					(% of span)	
Zero gas	0.0	0.0	0.0	0.0	0.0	0.0
Mid-range	450	450	0.0	446	0.8	0.8

Run No. 3

Date/Time 4/10/90 - 1554-1702

	Analyzer Calibration Response	Initial values		Final values		
		System Calibration Response	System bias (% of span)	System Calibration Response	System bias	Drift
					(% of span)	
Zero gas	0.0	0.0	0.0	0.0	0.0	0.0
Mid-range	450	450	0.0	450	0.0	0.0

System calibration bias = $\frac{\text{System calibration response} - \text{Analyzer calibration response}}{\text{Span}} \times 100$

Drift = $\frac{\text{Final system response} - \text{Initial system calibration response response}}{\text{Span}} \times 100$



Galson
-Technical Services

Comments:

PRE-TEST & POST-TEST SYSTEM DATA

Plant I. D. CCCSO

Project No. SE 7034

Source Incinerator #2

Operator THK

Pollutant CO

Analyzer I. D. TEO-48

Run No. 4

Date/Time 4/11/90 - 1027-1240

Run No. _____

	Analyzer Calibration Response	Initial values		Final values		Drift
		System Calibration Response	System bias (% of span)	System Calibration Response	System bias	
					(% of span)	
Zero gas	0	0.0	0.0	0.0	0.0	0.0
Mid-range	160	160	0.0	157	1.5	1.5

1119 - 1621

Run No. 5

Date/Time 4/11/90 - 1410 - 1621

Run No. 5

	Analyzer Calibration Response	Initial values		Final values		
		System Calibration Response	System bias (% of span)	System Calibration Response	System bias	Drift
					(% of span)	
Zero gas	0	0	0.0	0.0	0.0	0.0
Mid-range	160	160	0.0	154	0.6	0.6

102-1833-1050

Run No. 6

Date/Time 4/12/90 - 0833-1050

Run No. <u>6</u>	Initial values			Final values		
	Analyzer Calibration Response	System Calibration Response	System bias (% of span)	System Calibration Response	System bias	Drift
					(% of span)	
Zero gas	0	0	0			
Mid-range	160	160	0	157	1.5	1.5

System calibration bias = $\frac{\text{System calibration response} - \text{Analyzer calibration response}}{\text{Span}} \times 100$

Drift = $\frac{\text{Final system response} - \text{Initial system calibration response}}{\text{Span}} \times 100$



Galson
-Technical Services

Comments:

PRE-TEST & POST-TEST SYSTEM DRIFT CHECKS

Plant I. D. CCCS Project No. SE-034
Source Incin. #2 Operator MA
Pollutant CO Analyzer I. D. TECO-48

Run No. #7 Date/Time 4/12/90-1219-1546

	Analyzer Calibration Response	Initial values		Final values		Drift
		System Calibration Response	System bias (% of span)	System Calibration Response	System bias (% of span)	
Zero gas	0	0	0	—	—	—
Mid-range	160	160	0.0	158	1.0	1.0

Run No. 8 Date/Time 4/12/90-1645-2005

	Analyzer Calibration Response	Initial values		Final values		Drift
		System Calibration Response	System bias (% of span)	System Calibration Response	System bias (% of span)	
Zero gas	0	0	0	0	0	0
Mid-range	160	160	0.0	157	1.5	1.5

Run No. 9 Date/Time 4/13/90-1040-1340

	Analyzer Calibration Response	Initial values		Final values		Drift
		System Calibration Response	System bias (% of span)	System Calibration Response	System bias (% of span)	
Zero gas	0	0	0	—	—	—
Mid-range	160	160	0	158	1.0	1.0

System calibration bias = $\frac{\text{System calibration response} - \text{Analyzer calibration response}}{\text{Span}} \times 100$

Drift = $\frac{\text{Final system response} - \text{Initial system calibration response response}}{\text{Span}} \times 100$



Galson
Technical Services

PRE-TEST & POST-TEST SYSTEM DRIFT CHECKS

Plant I. D. CCCSO Project No. SE-034
Source Incin #2 Operator TH
Pollutant CO Analyzer I. D. TEC-48

Comments:

Run No. 10

Date/Time 4/13/90 - 1455-1823

	Initial values			Final values		
	Analyzer Calibration Response	System Calibration Response	System bias (% of span)	System Calibration Response	System bias	Drift
					(% of span)	
Zero gas	0.0	0.0	0.0	0.0	0.0	0.0
Mid-range	160	160	0.0	160	0.0	0.0

Run No. _____

Date/Time _____

	Initial values			Final values		
	Analyzer Calibration Response	System Calibration Response	System bias (% of span)	System Calibration Response	System bias	Drift
					(% of span)	
Zero gas						
Mid-range						

Run No. _____

Date/Time _____

	Initial values			Final values		
	Analyzer Calibration Response	System Calibration Response	System bias (% of span)	System Calibration Response	System bias	Drift
					(% of span)	
Zero gas						
Mid-range						

$$\text{System calibration bias} = \frac{\text{System calibration response} - \text{Analyzer calibration response}}{\text{Span}} \times 100$$

$$\text{Drift} = \frac{\text{Final system response} - \text{Initial system calibration response response}}{\text{Span}} \times 100$$



Galson
Technical Services

PRE-TEST & POST-TEST SYSTEM DRIFT CHECKS

Plant I. D. CCCSO Project No. SE-084
Source Incinert #2 Operator 3/11
Pollutant THC Analyzer I. D. Raffsch B-55

Comments:

Run No. 1

Date/Time 4/10/90 - 1158 - 1245

	Analyzer Calibration Response	Initial values		Final values		Drift
		System Calibration Response	System bias (% of span)	System Calibration Response	System bias	
					(% of span)	
Zero gas	0.0	0.0	0.0	0.5	0.5	0.5
Mid-range	45	45	0.0	46.5	1.5	1.5

Run No. 2

Date/Time 4/10/90 - 1357 - 1505

	Analyzer Calibration Response	Initial values		Final values		Drift
		System Calibration Response	System bias (% of span)	System Calibration Response	System bias	
					(% of span)	
Zero gas	0.0	0.0	0.0	-0.5	0.5	0.5
Mid-range	45	45	0.0	44.5	0.5	0.5

Run No. 3

Date/Time 4/10/90 - 1554 - 1702

	Analyzer Calibration Response	Initial values		Final values		Drift
		System Calibration Response	System bias (% of span)	System Calibration Response	System bias	
					(% of span)	
Zero gas	0.0	0.0	0.0	0.5	0.5	0.5
Mid-range	45	45	0.0	45	0.0	0.0

System calibration bias = $\frac{\text{System calibration response} - \text{Analyzer calibration response}}{\text{Span}} \times 100$

Drift = $\frac{\text{Final system response} - \text{Initial system calibration response response}}{\text{Span}} \times 100$



Galson
-Technical Services

Comments:

PRE-TEST & POST-TEST SYSTEM DRIFT CHECKS

Plant I. D. CCCSO Project No. SE-084
Source Incinerator # 2 Operator 7/1/90
Pollutant THC Analyzer I. D. Rafsch 255

Run No. 4

Date/Time 4/11/90 - 10³⁷ - 1240

	Initial values			Final values		
	Analyzer Calibration Response	System Calibration Response	System bias (% of span)	System Calibration Response	System bias	Drift
					(% of span)	
Zero gas	0.0	0.0	0.0	2.5	2.5	2.5
Mid-range	7.9	7.9	0.0	10	2.1	2.1

Run No. 5

Date/Time 4/11/90 - 14¹⁰ - 1621

	Initial values			Final values		
	Analyzer Calibration Response	System Calibration Response	System bias (% of span)	System Calibration Response	System bias	Drift
					(% of span)	
Zero gas	0.0	0.0	0.0	0.0	0.0	0.0
Mid-range	45	45	0.0	44.5	154	0.5

Run No. 6

Date/Time 4/12/90 - 0833 - 050

	Initial values			Final values		
	Analyzer Calibration Response	System Calibration Response	System bias (% of span)	System Calibration Response	System bias	Drift
					(% of span)	
Zero gas	0	0	0	2	2	2
Mid-range	45	45	0.0	45	0	0

System calibration bias = $\frac{\text{System calibration response} - \text{Analyzer calibration response}}{\text{Span}} \times 100$

Drift = $\frac{\text{Final system response} - \text{Initial system calibration response}}{\text{Span}} \times 100$



Galson
-Technical Services

PRE-TEST & POST-TEST SYSTEM DRIFT CHECKS

Plant I. D. CCCSO Project No. SE-034
Source Incinerator #2 Operator [Signature]
Pollutant TlTC Analyzer I. D. Raffish RS-55

Comments:

Run No. #7

Date/Time 4/12/90 - 1219-1546

	Initial values			Final values		
	Analyzer Calibration Response	System Calibration Response	System bias (% of span)	System Calibration Response	System bias	Drift
					(% of span)	
Zero gas	0	0	0	2.5	2.5	2.5
Mid-range	45	45	0	44.5	0.5	0.5

Run No. #8

Date/Time 4/12/90 - 1645-2005

	Initial values			Final values		
	Analyzer Calibration Response	System Calibration Response	System bias (% of span)	System Calibration Response	System bias	Drift
					(% of span)	
Zero gas	0	0	0	0	0	0
Mid-range	45	45	0	45	0	0

Run No. 9

Date/Time 4/12/90 - 1010-1340

	Initial values			Final values		
	Analyzer Calibration Response	System Calibration Response	System bias (% of span)	System Calibration Response	System bias	Drift
					(% of span)	
Zero gas	0	0	0	—	—	—
Mid-range	45	45	0	46	1.0	1.0

$$\text{System calibration bias} = \frac{\text{System calibration response} - \text{Analyzer calibration response}}{\text{Span}} \times 100$$

$$\text{Drift} = \frac{\text{Final system response} - \text{Initial system calibration response}}{\text{Span}} \times 100$$



PRE-TEST & POST-TEST SYSTEM DRIFT CHECKS

Plant I. D. CCCSO Project No. SE-034
 Source Incin. # 2 Operator MA
 Pollutant THC Analyzer I. D. Katish RS-55

Comments:

Run No. 10

Date/Time 4/13/91-1455-1803

	Analyzer Calibration Response	Initial values		Final values		Drift
		System Calibration Response	System bias (% of span)	System Calibration Response	System bias	
					(% of span)	
Zero gas	0.0	—	—	-1.0	1.0	1.0
Mid-range	45	45	0.0	45	0.0	0.0

Run No. _____

Date/Time _____

	Analyzer Calibration Response	Initial values		Final values		Drift
		System Calibration Response	System bias (% of span)	System Calibration Response	System bias	
					(% of span)	
Zero gas						
Mid-range						

Run No. _____

Date/Time _____

	Analyzer Calibration Response	Initial values		Final values		Drift
		System Calibration Response	System bias (% of span)	System Calibration Response	System bias	
					(% of span)	
Zero gas						
Mid-range						

$$\text{System calibration bias} = \frac{\text{System calibration response} - \text{Analyzer calibration response}}{\text{Span}} \times 100$$

$$\text{Drift} = \frac{\text{Final system response} - \text{Initial system calibration response response}}{\text{Span}} \times 100$$

APPENDIX V: FIELD DATA AND CALCULATIONS

NOMENCLATURE

A(N)	- CROSS-SECTIONAL AREA OF NOZZLE, FT ²
CFH	- CUBIC FEET PER HOUR
CFM	- CUBIC FEET PER MINUTE
FT ²	- SQUARE FEET
FT ³	- CUBIC FEET
FPM	- FEET PER MINUTE
GAMMA	- DRY GAS METER CALIBRATION FACTOR
GMS	- GRAMS
GR/DSCF	- GRAINS PER DRY STANDARD CUBIC FOOT
HG	- MERCURY
ΔH	- PRESSURE DROP ACROSS THE ORIFICE METER, INCHES OF H ₂ O
IN HG	- INCHES OF MERCURY
P(BAR)	- BAROMETRIC PRESSURE, INCHES HG
P(BAR)+(ΔH/13.6)	- METER PRESSURE, INCHES HG
P(S)	- PRESSURE IN STACK, INCHES HG
P	- VELOCITY PRESSURE, INCHES H ₂ O
°R	- 460 + °F
SCF	- STANDARD CUBIC FOOT
SCFM	- STANDARD CUBIC FOOT PER MINUTE
T(M)	- AVERAGE DRY GAS METER TEMPERATURE, °R
THETA	- TOTAL SAMPLE TIME, MINUTES
T(S)	- AVERAGE STACK TEMPERATURE, °R
V(LC)	- TOTAL VOLUME OF LIQUID COLLECTED IN IMPINGERS AND SILICA GEL, ML
V(M)	- VOLUME OF GAS SAMPLED (METER CONDITIONS), FT ³
V(S)	- AVERAGE STACK GAS VELOCITY, FT/MIN
13.6	- SPECIFIC GRAVITY OF MERCURY

HCl Emission Data

SUMMARY OF TEST DATA - HCl EMISSIONS

PLANT: CCCSD	STACK #: INCINERATOR #2 EXHAUST		
	RUN#1	RUN#2	RUN#3
NUMBER OF SAMPLING POINTS	24	24	24
DURATION OF THE RUN, MINUTES	60	60	60
SAMPLING NOZZLE DIAMETER, INCHES	0.213	0.213	0.213
PITOT CALIBRATION FACTOR (CF)	0.84	0.84	0.84
METER CALIBRATION FACTOR, GAMMA	1.006	1.006	1.006
STACK DIAMETER, INCHES	41	41	41
AMBIENT AIR TEMPERATURE, °F	65	75	70
BAROMETRIC PRESSURE, INCHES HG	30.08	30.08	30.08
AVG STATIC PRES IN FLUE, INCHES H ₂ O	-0.11	-0.11	-0.22
ABSOLUTE PRES IN FLUE (P(S)), INCHES HG	30.07	30.07	30.06
AVG STACK VELOCITY HEAD (SQRT(ΔP))	0.688	0.699	0.720
AVERAGE ORIFICE (ΔH), INCHES H ₂ O	0.74	0.76	0.81
VOL SAMPLED (V(M)), FT ³ (METER COND)	29.90	30.02	30.43
AVERAGE STACK TEMPERATURE (T(S)), °F	152	156	156
AVERAGE IMPINGER OUTLET TEMP, °F	73	85	74
AVERAGE METER TEMPERATURE, °F	93	89	82
AVERAGE METER VACUUM, INCHES HG	2.0	2.5	2.5
VOLUME OF WATER CONDENSED (V(LC)), ML	18.1	15.6	17.1
SPECIFIC GRAVITY OF FLUE GAS (SG)	1.004	1.009	1.007
HYDROGEN CHLORIDE COLLECTED, MG	0.39	0.46	0.51
ORSAT ANALYSIS:			
%CO ₂	5.1	5.6	5.4
%O ₂	14.7	14.6	14.6
%CO	0.0	0.0	0.0

SUMMARY OF TEST DATA - HCl EMISSIONS

PLANT: CCCSD

STACK #: INCINERATOR #2 EXHAUST

	<u>RUN#1</u>	<u>RUN#2</u>	<u>RUN#3</u>
A. AREA OF STACK, FT ²	9.17	9.17	9.17
B. VOLUME SAMPLED (METER COND.), FT ³	29.90	30.02	30.43
C. VOLUME SAMPLED (STANDARD COND.), FT ³ $\frac{B \cdot \text{GAMMA} \cdot P(\text{BAR}) + (\Delta H / 13.6) \cdot 530}{[(29.92) \cdot T(M)]}$	29.02	29.36	30.14
D. VOLUME OF LIQUID WATER CONDENSED, ML	18.1	15.6	17.1
E. VAPOR VOLUME OF WATER CONDENSED, SCF (STD. CONDITIONS), D°0.04728	0.86	0.74	0.81
F. MOISTURE, %, (E/(E+C))*100	2.86	2.45	2.61
G. AVERAGE VELOCITY IN THE STACK, FPM $\frac{4005 \cdot (\text{SQRT}(\Delta P)) \cdot \text{CF} \cdot \text{SQRT}((T(S) \cdot 29.92 \cdot 1.0) / (530 \cdot P(S) \cdot \text{SG}))}{\text{A} \cdot \text{G}}$	2,475	2,518	2,597
H. STACK GAS FLOW RATE (STACK COND.), CFM A°G	22,694	23,085	23,806
J. STACK GAS FLOW RATE (STANDARD CONDITIONS, DRY STATE), DSCFM $H \cdot (1 - (F/100)) \cdot (530/T(S)) \cdot (P(S)/29.92)$	19,191	19,475	20,038
K. HYDROGEN CHLORIDE COLLECTED, MG	0.39	0.46	0.51
L. HYDROGEN CHLORIDE CONC., MG/DSCM (K°35.3/C)	0.474	0.553	0.597
M. HYDROGEN CHLORIDE EMISSION RATE, GM/HR $[(L \cdot J \cdot 60) \cdot 10^{-3}] / 35.3$	15.5	18.3	20.3
N. SLUDGE FEED RATE, TONS/HR (DRY)	1.7	1.6	1.7
O. HYDROGEN CHLORIDE EMISSION RATIO, GM/TON M / N	9.10	11.44	11.97

ORSAT DATA AND GAS DENSITY CALCULATIONS

PLANT: CCCSD

STACK #: INCINERATOR #2 EXHAUST

	<u>RUN #1</u>		<u>RUN #2</u>		<u>RUN #3</u>	
<u>PARAMETER</u>	<u>DRY BASIS</u>	<u>WET BASIS</u>	<u>DRY BASIS</u>	<u>WET BASIS</u>	<u>DRY BASIS</u>	<u>WET BASIS</u>
CO ₂	5.10	4.95	5.60	5.46	5.40	5.26
O ₂	14.70	14.28	14.60	14.24	14.60	14.22
CO	0	0	0	0	0	0
N ₂	80.20	77.90	79.80	77.84	80.00	77.91
H ₂ O	- -	2.86	- -	2.45	- -	2.61
MOLECULAR WEIGHT ¹	- -	29.08	- -	29.20	- -	29.15
SPECIFIC GRAVITY OF GAS ²	- -	1.004	- -	1.009	- -	1.007

¹ CALCULATED FROM THE EQUATION:

MOLECULAR WEIGHT = $0.44(\%CO_2) + 0.32(\%O_2) + 0.28(\%N_2 + \%CO) + 0.18(\%H_2O)$

² SG = MOLECULAR WEIGHT STACK GAS / MOLECULAR WEIGHT OF AIR (28.95 GM/MOLE)

ISOKINETIC VARIATION CALCULATION

PLANT: CCCSD

STACK #: INCINERATOR #2 EXHAUST

PARAMETER	RUN #1	RUN #2	RUN #3
T(S), °R	612	616	616
V(LC), ML	18.1	15.6	17.1
GAMMA	1.006	1.006	1.006
V(M), FT ³	29.90	30.02	30.43
T(M), °R	553	549	542
P(BAR)+(ΔH/13.6), IN HG	30.13	30.14	30.14
V(S), FPM	2,475	2,518	2,597
P(S), IN HG	30.07	30.07	30.06
A(N), FT ²	0.00025	0.00025	0.00025
THETA, MINUTES	60	60	60
I (PERCENT OF ISOKINETIC) ^a	93.4	93.1	92.9

$$^a I = \frac{(T(S)(AVG) \cdot 100((0.00267 \cdot V(CL)) + (V(M)/T(M)) \cdot GAMMA \cdot (P(BAR) + (\Delta H/13.6))))}{(THETA \cdot V(S) \cdot P(S) \cdot A(N))}$$

1/2



Comments: CE
1.23 175
1.19 150
1.14 175
1.09 100

SAMPLE COLLECTION DATA

Plant CCCSO-AB2388
 Location 4/10/10
 Date 4/10/10
 Run Number 1- HCL
 Operator 1- HCL
 Sample Box ID 002
 Meter Box ID 005
 Probe ID 2
 Filter # 3

Meter ID 1006
 Meter ΔH@ 1.20
 Pilot C.F. 0.25
 Assumed Moisture % 5%
 Nozzle Diameter in. 0.213
 C Factor 1.20
 Ambient Temperature 65
 Barometric Pressure 30.08
 Silica Gel # 3

Static Pressure: Y44 x A10
 Traverse Pt. 0.25
 Pstatic 0.25
 Water Collected: 205-200
 Impingers, ml. 5
 Silica Gel, gms. 13.1
16.1

V-222793

02-51 102-14.1

Traverse Point (Number)	Sampling Time min.	Stack Temp. (Ts) °F	Stack ΔP in. H2O	Orifice ΔH in. H2O	Meter Reading (Vm) ft3	Dry Gas Meter Temp.		Sample Box Temp. °F	Probe Temp. °F	Impinger Outlet °F	Pump Vac. in Hg.
						T in °F	T out °F				
1	2.5	159	0.43	0.62	—	77	84	252	236	75	<2
2	5	158	0.47	0.71	230.2	79	84	252	230	75	<2
3	7.5	163	0.55	0.84	—	81	84	250	224	74	<2
4	10	168	0.51	0.79	—	84	84	250	222	72	<2
5	12.5	165	0.51	0.79	234.1	86	84	251	222	70	<2
6	15	165	0.53	0.81	235.5	89	84	250	223	70	<2
7	17.5	154	0.53	0.81	236.7	91	85	250	224	69	<2
8	20	154	0.53	0.81	—	94	86	250	226	69	<2
9	22.5	151	0.53	0.81	239.3	97	86	252	228	69	<2
10	25	151	0.50	0.76	242.6	99	88	250	230	67	<2
11	27.5	150	0.50	0.76	241.8	100	89	252	234	69	<2
12	30	153	0.49	0.76	243.0	100	90	250	236	68	<2
Averages											

5.38 11.0

5.38 12.0



Comments: Post Test
Leak Rate
0.006 cfm
@ 13 in Hg

SAMPLE COLLECTION DATA

Plant CCSP-AB2568
Location Unit 2
Date 4/10/90
Run Number 1-H3
Operator RR/KP
Sample Box ID 23-2
Meter Box ID 005
Probe ID 95
Filter # —

Meter ID 1006
Meter ΔH @ 6.73
Pilot C.F. 0.84
Assumed Moisture % 5
Nozzle Diameter in. 0.213
C Factor 1.20
Ambient Temperature 68
Barometric Pressure 30.08
Silica Gel # —

Order # 102

Static Pressure: 85
Traverse Pt. 0.18
Pwake —
Pstatic —
Water Collected: —
Impingers, ml. —
Silica Gel, gms. —

Traverse Point Number	Sampling Time min.	Stack Temp. (Ts) °F	Stack ΔP in. H2O	Orifice ΔH in. H2O	Meter Reading (Vm) ft3	Dry Gas Meter Temp.		Sample Box Temp. °F	Probe Temp. °F	Impinger Outlet °F	Pump Vac. in Hg.
						T in °F	T out °F				
1	32.5	118	0.20	0.34	—	90	91	250	200	75	<2
2	35	120	0.27	0.44	245.0	94	92	252	200	75	<2
3	37.5	124	0.34	0.52	—	96	92	252	214	79	<2
4	40	123	0.35	0.54	—	98	94	252	226	76	<2
* 5	42.5	128	0.38	0.58	248.2	100	94	252	235	76	<2
6	45	138	0.42	0.64	249.4	101	95	254	240	76	<2
7	47.5	164	0.51	0.80	—	103	96	254	244	76	<2
8	50	167	0.55	0.85	—	105	96	254	244	72	<2
9	52.5	158	0.58	0.89	253.4	107	97	256	246	74	<2
10	55	170	0.62	0.95	—	109	99	256	249	75	<2
4511	57.5	168	0.64	0.98	256.3	111	100	256	250	78	<2
12	60	176	0.59	0.90	—	111	100	257	251	76	<2
				$V_c = 257.692$							
Averages		151.88	0.688	0.74	249.90	93.23		252.25	230.58	73.21	2.0



Galson
Technical Services

Comments:

1/2

SAMPLE COLLECTION DATA

Plant CCCSO
Location Unit 12 stack
Date 4/10/90
Run Number 2-HCI
Operator DR/KP
Sample Box ID 205-2
Meter Box ID 205
Probe ID 4 sheathed
Filter # _____

Meter 1.006
Meter ΔH @ 1.72
Pilot C.F. 0.84
Assumed Moisture % _____
Nozzle Diameter in. 3.313
C Factor 1.20
Ambient Temperature 75
Barometric Pressure 30.28
Silica Gel # _____

$V_i = 257.922$ 0.391 # 0.9

Traverse Point Number	Sampling Time min.	Stack Temp. (Ts) °F	Stack ΔP in. H ₂ O	Orifice ΔH in. H ₂ O	Meter Reading (V _m) ft ³	Dry Gas Meter Temp.		Sample Box Temp. °F	Probe Temp. °F	Impinger Outlet °F	Pump Vac. in Hg.
						T in °F	T out °F				
1 <u>B1</u>	<u>2.5</u>	<u>122</u>	<u>0.30</u>	<u>0.46</u>	<u>258.9</u>	<u>82</u>	<u>90</u>	<u>240</u>	<u>244</u>	<u>82</u>	<u>2</u>
2	<u>5</u>	<u>123</u>	<u>0.33</u>	<u>0.49</u>	<u>260.0</u>	<u>83</u>	<u>89</u>	<u>242</u>	<u>242</u>	<u>85</u>	<u>2</u>
3	<u>7.5</u>	<u>123</u>	<u>0.34</u>	<u>0.52</u>	—	<u>85</u>	<u>89</u>	<u>243</u>	<u>226</u>	<u>86</u>	<u>2</u>
4	<u>10</u>	<u>128</u>	<u>0.38</u>	<u>0.59</u>	<u>262.1</u>	<u>89</u>	<u>89</u>	<u>240</u>	<u>221</u>	<u>89</u>	<u>2</u>
5	<u>12.5</u>	<u>128</u>	<u>0.37</u>	<u>0.57</u>	—	<u>91</u>	<u>89</u>	<u>241</u>	<u>222</u>	<u>87</u>	<u>2</u>
6	<u>15</u>	<u>136</u>	<u>0.41</u>	<u>0.62</u>	—	<u>91</u>	<u>89</u>	<u>239</u>	<u>223</u>	<u>88</u>	<u>2</u>
7	<u>17.5</u>	<u>169</u>	<u>0.52</u>	<u>0.80</u>	<u>265.7</u>	<u>91</u>	<u>89</u>	<u>238</u>	<u>224</u>	<u>84</u>	<u>2</u>
8	<u>20</u>	<u>174</u>	<u>0.57</u>	<u>0.86</u>	<u>267.0</u>	<u>91</u>	<u>89</u>	<u>236</u>	<u>223</u>	<u>80</u>	<u>2.5</u>
9	<u>22.5</u>	<u>176</u>	<u>0.61</u>	<u>0.94</u>	<u>268.4</u>	<u>91</u>	<u>89</u>	<u>234</u>	<u>225</u>	<u>78</u>	<u>3</u>
10	<u>25</u>	<u>177</u>	<u>0.64</u>	<u>0.98</u>	<u>269.8</u>	<u>92</u>	<u>89</u>	<u>234</u>	<u>222</u>	<u>79</u>	<u>3</u>
11	<u>27.5</u>	<u>175</u>	<u>0.64</u>	<u>0.98</u>	<u>271.2</u>	<u>93</u>	<u>89</u>	<u>232</u>	<u>223</u>	<u>78</u>	<u>3</u>
12	<u>30</u>	<u>175</u>	<u>0.62</u>	<u>0.96</u>	<u>272.64</u>	<u>93</u>	<u>89</u>	<u>232</u>	<u>225</u>	<u>80</u>	<u>3</u>

Static Pressure:

Traverse Pt. 1.84

Pwake -0.22

Pstatic _____

Water Collected:

Impingers, ml. 205-200

Silica Gel, gms. 9.6

CO₂ 5.6 O₂ 13.6

2/2



Galson
Technical Services

Comments:
Post test leak
Rate 0.004cfm
@ 12 in Hg

SAMPLE COLLECTION DATA

Plant CCCSP-AB2588 Meter 0 1006

Location Unit 2560 Meter ΔH 172

Date 4/10/90 Pilot C.F. 0.84

Run Number 2-HC1 Assumed Moisture % 5

Operator DR/KP Nozzle Diameter in. 0.213

Sample Box ID 08-2 C Factor 1.20

Meter Box ID 005 Ambient Temperature 75

Probe ID 4 Barometric Pressure 30.09

Filter # _____ Silica Gel # _____

Static Pressure:

Traverse Pt. *84 B7

Pwake 0.22 0.30

Pstatic _____

Water Collected: _____

Impingers, ml. _____

Silica Gel, gms. _____

Traverse Point Number	Sampling Time min.	Stack Temp. (T _s) °F	Stack ΔP in. H ₂ O	Orifice ΔH in. H ₂ O	Meter Reading (V _m) ft ³	Dry Gas Meter Temp.		Sample Box Temp. °F	Probe Temp. °F	Impinger Outlet °F	Pump Vac. in Hg.
						T in °F	T out °F				
A1	32.5	135	0.38	0.53	273.8	83	89	232	227	80	2
A2	35	165	0.50	0.77	275.0	85	88	234	230	86	2
3	27.5	170	0.50	0.77	—	86	88	235	232	86	2
*4	40	174	0.46	0.71	277.5	89	89	236	233	88	2
5	42.5	172	0.44	0.65	278.7	89	89	236	234	88	2
6	45	166	0.53	0.81	280.0	89	89	237	234	86	2.5
*7	47.5	162	0.58	0.90	—	90	89	236	233	87	3
8	50	161	0.57	0.88	282.6	91	89	237	234	88	3
9	52.5	159	0.57	0.88	284.0	91	89	238	234	88	3
10	55	158	0.56	0.86	285.3	91	89	238	234	86	3
11	57.5	158	0.55	0.84	286.7	91	89	238	234	86	3
12	60	157	0.50	0.77	287.94	91	89	238	235	85	3
Averages		155.96	0.699	0.76	30.02	89.02		236.92	229.75	84.58	2.46

5.05
2.3

5.08
3.0



Comments:

SAMPLE COLLECTION DATA

Plant CCCSO
Location Unit 2 Stack
Date 4/19/90
Run Number 3-H11
Operator OR/KP
Sample Box ID 003-2
Meter Box ID 4,002
Probe ID 4,002
Filter # 288.088

Meter ID 1.006
Meter ΔH @ 1.72
Pilot C.F. 0.84
Assumed Moisture % 3
Nozzle Diameter in. 0.313
C Factor 1.20
Ambient Temperature 70
Barometric Pressure 30.08
Silica Gel # 0.547 # 06

Static Pressure:

Traverse Pt. 14 247
Pwake -0.30 -0.50
Pstatic _____

Water Collected:

210-200
Impingers, ml. 10
Silica Gel, gms. 7.1 17.1

0.547 0.547

Traverse Point Number	Sampling Time min.	Stack Temp. (Ts) °F	Stack ΔP in. H2O	Orifices ΔH in. H2O	Meter Reading (Vm) ft3	Dry Gas Meter Temp.		Sample Box Temp. °F	Probe Temp. °F	Impinger Outlet °F	Pump Vac. in Hg.
						T in °F	T out °F				
A1	2.5	176	0.45	0.69	289.2	76	82	237	235	74	2
2	5	183	0.48	0.76	290.5	78	82	232	235	74	2
3	7.5	180	0.50	0.77	291.7	74	82	228	232	79	2
* 4	10	180	0.50	0.77	—	80	82	224	231	80	2
5	12.5	176	0.44	0.68	294.1	82	81	225	231	77	2
6	15	170	0.54	0.83	295.4	83	81	226	230	78	2
* 7	17.5	161	0.67	1.00	296.8	84	82	229	230	77	3
8	20	158	0.66	1.00	298.2	85	81	230	229	76	3
9	22.5	156	0.65	1.00	299.7	86	82	232	228	76	3
10	25	153	0.63	0.96	301.0	86	82	233	226	74	3
11	27.5	150	0.61	0.94	302.4	86	82	235	224	74	3
12	30	153	0.62	0.95	303.827	87	82	235	223	73	3
Averages											

3:54

10:54



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Technical Services

Comments: Post Test
Leak Rate 0.0004cfm
@ QinHg

SAMPLE COLLECTION DATA

2/2

Plant CCSD
Location Unit 2 Stack
Date 4/10/90
Run Number 3 HCL
Operator DR/KP
Sample Box ID 08-3
Meter Box ID 005
Probe ID 4
Filter #

Meter Ø 1006
Meter ΔH @ 1.72
Pilot C.F. 0.84
Assumed Moisture % 5
Nozzle Diameter in. 0.213
C Factor 1.20
Ambient Temperature 70
Barometric Pressure 30.02
Silica Gel #

Static Pressure:

Traverse Pt B6

Pwake -0.30

Pstatic

Water Collected:

Impingers, ml.

Silica Gel, gms.

Traverse Point Number	Sampling Time min.	Stack Temp. (Ts) °F	Stack ΔP in. H ₂ O	Orifice ΔH in. H ₂ O	Meter Reading (V _m) ft ³	Dry Gas Meter Temp.		Sample Box Temp. °F	Probe Temp. °F	Impinger Outlet °F	Pump Vac. in Hg.
						T in °F	T out °F				
01	32.5	100	0.24	0.37	—	77	81	234	210	68	2
2	35	110	0.37	0.57	305.8	78	81	235	210	70	2
3	37.5	118	0.37	0.57	306.9	79	81	235	211	71	3
4	40	120	0.38	0.59	308.0	80	80	233	213	72	2
5	32.5	126	0.40	0.62	309.1	81	81	234	219	74	2
6	45	137	0.45	0.69	310.3	83	81	236	222	74	—
7	47.5	168	0.55	0.85	311.6	84	81	236	224	74	2
8	50	168	0.57	0.88	312.9	85	81	237	226	74	3
9	52.5	174	0.63	0.97	314.3	87	81	238	229	74	3
10	55	176	0.64	0.99	315.7	88	82	240	231	73	3
11	57.5	175	0.63	0.97	317.1	89	82	240	233	73	3
12	60	175	0.64	0.99	318.517	90	82	241	233	72	3
Averages		156.17	0.72	0.81	30.43	82.25		233.54	225.63	74.42	2.48

FLUE GAS ANALYSES FIELD DATA

Plant ID: CCCSO

Date: 4/10/90

Quality Control

Leak check - all components must pass

O₂/QC gas analysis results

Pre-test	Post-test	Gas ID	Run #	CO ₂	CO ₂ +O ₂	O ₂	CO
☒ CO ₂ Pipette	☐		1				
☒ O ₂ pipette	☐		2				
☒ CO pipette	☐		3				
☒ Sample burette	☐						

ORSAT ANALYSES DATA

Sample Bag ID	CO ₂ %	CO ₂ + O ₂	O ₂ %	CO ₂ + O ₂ + CO	CO %	Fe
#102 (Test)	a) 5.0 5.2	20.2 20.0	14.8			
	b) 5.1 5.0	19.8 19.6	14.6			
	c) 5.1	20.4				
	1) 5.0	19.8	14.8			
	Aug 5.1		14.7			
#09	a) 5.6	20.1	14.5			
	b) 5.7	20.3	14.6			
	c) 5.6	20.2	14.6			
	Aug 5.6		14.6			
#06	a) 5.1	19.6	14.3			
	b) 5.4	20.0	14.6			
	c) 5.4	20.1	14.7			
	Aug 5.4		14.6			

**Formaldehyde, Benzene, and Vinyl Chloride
Emission Data**

SUMMARY OF TEST DATA - FORMALDEHYDE EMISSIONS

Plant: CCCSD

Stack: Incinerator #2 Exhaust

Sampling Data:

	Run #1	Run #2	Run #3
Test Duration, minutes	60	60	60
Ambient Air Temperature, °F	65	65	65
Barometric Pressure (Pbar), inches Hg	30.08	30.08	30.08
Avg Orifice Temp at Calibration (Toc), °F	67.0	67.5	67.0
Avg Orifice Temp at Test (To), °F	67.0	68.0	68.1
Avg Sampling Rate at Calibration, l/min	0.432	0.527	0.542
Stack Gas Flow Rate ¹ (dscfm)	19,191	19,475	20,038
Formaldehyde Collected ² , µg	2.59	0.85	2.00

Calculations:

A. Avg. Sampling Rate (Cal. Conditions), l/min	0.432	0.527	0.542
B. Avg. Sampling Rate (Test Conditions), l/min A*SQRT(To/Toc)	0.432	0.528	0.542
C. Volume Sampled (Test Conditions), l B*Test Duration	25.9	31.7	32.5
D. Volume Sampled (Std. Conditions), ft ³ (C/28.32)*(Pbar/29.92)*(528/To)	0.925	1.128	1.159
E. Stack Gas Flow Rate, dscfm	19,191	19,475	20,038
F. Formaldehyde Collected, µg	2.59	0.85	2.00
G. Formaldehyde Concentration, mg/dscm F*35.3/(D*1000)	0.099	0.027	0.061
H. Formaldehyde Concentration, ppm (G*24.13)/30 ³	0.080	0.021	0.049
I. Formaldehyde Emission Rate, gms/hr (G*E*60)/(1000*35.3)	3.22	0.88	2.07
J. Sludge Feed Rate, tons/hr (dry)	1.7	1.6	1.7
K. Formaldehyde Emission Ratio, gms/ton (dry), I / J	1.90	0.55	1.22

¹ Based on flow rate data collected concurrently during the HCl testing.

² Formaldehyde quantities are corrected for the blank; refer to the laboratory data presented in Appendix VI for details.

³ Molecular weight of formaldehyde = 30 gm/gm-mole.

FIELD DATA - CRITICAL ORIFICE

PLANT CCSD RUN No. #2 AMBIENT TEMP. (°F) 65
LOCATION Unit 2 - Stack CONTAMINANTS Formaldehyde BARO. PRESS. (in. Hg) 30.08
DATE 4/10/90 OPERATOR [Signature]

CALIBRATION DATA

CALIBRATION RUN No.	BURETTE VOL. (cc)	ORIFICE TEMP. (°F)	TIME (sec)
PRE-TEST - 1	150	67	16.31
2			16.48
3			16.47
AVG.			16.44

Flow (L/min) 0.5472

TEST DATA

CLOCK TIME	SAMPLING TIME (min)	FLOWMETER RDG.	ORIFICE TEMP ($^{\circ}$ F)
Start 2:57	1:57	5.8	68
	2:07	5.8	68
	2:17	5.8	68
	2:27	5.8	68
	2:37	5.8	68
Stop 2:57	2:55	5.8	68
	2:57		
Total	60	5.8	Avg. 68

POST-TEST-1	15	66	17.80
2			17.63
3			17.76
Avg.			17.730

Flow (ml/min): 0.5076

Average Flow (ml/min)	0.5274
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Technical Services, Inc.
Instrumental Services
Division

COMMENTS:

Yellowish Discoloration of
/orange Imp. ~~of~~ Sol'n

FIELD DATA – CRITICAL ORIFICE

PLANT CCCSO RUN No. #1 AMBIENT TEMP. (°F) 65
LOCATION Unit #2 Stack CONTAMINANTS Formaldehyde BARO. PRESS. (In. Hg) 30.08
DATE 4/10/90 OPERATOR DR

CALIBRATION DATA

CALIBRATION RUN No.	BURETTE VOL. (cc)	ORIFICE TEMP. (°F)	TIME (sec)
PRE-TEST-1	150	67	19.96
2			19.95
3			19.90
Avg.			19.90

FLOW (L/min) 0.4522



5.75

575

STOP 12:38pm

POST-TEST-1	150	67	21.97
2			21.80
3			21.82
Avg.			21.87

FLOW (L/min): 0.4115

Average Flow (l/min)	0.4319
-------------------------	--------

TEST DATA

CLOCK TIME	SAMPLING TIME (min)	FLOWMETER RDG.	ORIFICE TEMP ($^{\circ}$ F)
11:58	-	5.75	67
11:48	-	5.75	67
11:58	-	5.80	67
12:05	-	5.9	67
12:08	-	5.9	67
12:16	-	5.8	67
12:26	-	5.8	67
12:36	-	5.8	67
Total	60	~5.	Avg. 67

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Technical Services, Inc.
Environmental Sciences
Division

COMMENTS:

Buy #203

11

PLANT CCCSO RUN No. # 3 AMBIENT TEMP. (°F) 65
LOCATION Unit 2 Stack CONTAMINANTS Formaldehyde BARO. PRESS. (In. Hg) 30.08
DATE 4/10/90 OPERATOR gmk

TEST DATA

SALINATION RUN NO.	BURETTE VOL. (cc)	ORIFICE TEMP. (°F)	TIME (sec)
PRE-TEST-1	150	67	16.30
2			16.47
3			16.40
AVG.			16.390

Flow (L/min) 0.5491

POST-TEST-1	150	67	16.77
2			16.81
3			16.93
Avg.			16.837

FLOW (L/min): 0.5345

Average Flow (L/min)	0.5418
----------------------	--------

CLOCK TIME	SAMPLING TIME (min)	FLOWMETER RDG.	ORIFICE TEMP (°F)
3:54		1	68
4:01		5.8	69
4:15		5.8	68
4:22		5.8	68
4:31		5.7	68
4:37		5.7	68
4:41		5.7	68
4:43		5.7	68
4:54		5.7	68
Total	60	5.75	Avg. 68.1

Gabson

COMMENTS:

No Discoloration

SUMMARY OF TEST DATA- BENZENE AND VINYL CHLORIDE EMISSIONS

PLANT: CCCSD		STACK #: INCINERATOR #2 EXHAUST		
		<u>RUN #1</u>	<u>RUN #2</u>	<u>RUN#3B</u>
A. STACK GAS FLOW RATE ^a , DSCFM		19,191	19,475	20,038
B. CONCENTRATION, PPB				
• BENZENE		< 4.0	5.5	3.8
• VINYL CHLORIDE		< 4.0	< 4.0	< 2.0
C. EMISSION RATE, GM/HR (A*B*M ^b *60)/(10 ⁶ *35.3*24.13)				
• BENZENE		< 0.4	0.59	0.42
• VINYL CHLORIDE		< 0.3	< 0.3	< 0.2
D. SLUDGE FEED RATE, TONS/HR (DRY)		1.7	1.6	1.7
E. EMISSION RATIO, GM/TON (DRY) C / D				
• BENZENE		< 0.2	0.37	0.25
• VINYL CHLORIDE		< 0.2	< 0.2	< 0.1
^a Based on data collected concurrently during the HCl emission tests. ^b Molecular weight of benzene = 78 gm/gm-mole. Molecular weight of vinyl chloride = 62.5 gm/gm-mole.				

FIELD DATA – CRITICAL ORIFICE

PLANT CICSD-AB2588 RUN NO. 1 AMBIENT TEMP. (°F) 65
LOCATION Unit 2 stack CONTAMINANTS Benzene BARO. PRESS. (in. Hg) 30.08
DATE _____ VINYL CHLORIDE _____ OPERATOR WPK

CALIBRATION DATA

SOLUTION NUM No.	BURETTE VOL. (cc)	ORIFICE TEMP. (°F)	TIME (sec)
PRE-TEST - 1			
2			
3			
Av.			

Flow (Aval)

TEST DATA

CLOCK TIME	SAMPLING TIME (min)	FLOWMETER RDG.	ORIFICE TEMP (°F)
11:39			
12:29			
Total			Avg.

Start

Stop.

POST-TEST-1			
2			
3			
Avg.			

FLOW (L/min):

Average Flow (M/min)	
0.00	0.00
0.05	0.05
0.10	0.10
0.15	0.15
0.20	0.20
0.25	0.25
0.30	0.30
0.35	0.35
0.40	0.40
0.45	0.45
0.50	0.50
0.55	0.55
0.60	0.60
0.65	0.65
0.70	0.70
0.75	0.75
0.80	0.80
0.85	0.85
0.90	0.90
0.95	0.95
1.00	1.00
1.05	1.05
1.10	1.10
1.15	1.15
1.20	1.20
1.25	1.25
1.30	1.30
1.35	1.35
1.40	1.40
1.45	1.45
1.50	1.50
1.55	1.55
1.60	1.60
1.65	1.65
1.70	1.70
1.75	1.75
1.80	1.80
1.85	1.85
1.90	1.90
1.95	1.95
2.00	2.00
2.05	2.05
2.10	2.10
2.15	2.15
2.20	2.20
2.25	2.25
2.30	2.30
2.35	2.35
2.40	2.40
2.45	2.45
2.50	2.50
2.55	2.55
2.60	2.60
2.65	2.65
2.70	2.70
2.75	2.75
2.80	2.80
2.85	2.85
2.90	2.90
2.95	2.95
3.00	3.00
3.05	3.05
3.10	3.10
3.15	3.15
3.20	3.20
3.25	3.25
3.30	3.30
3.35	3.35
3.40	3.40
3.45	3.45
3.50	3.50
3.55	3.55
3.60	3.60
3.65	3.65
3.70	3.70
3.75	3.75
3.80	3.80
3.85	3.85
3.90	3.90
3.95	3.95
4.00	4.00
4.05	4.05
4.10	4.10
4.15	4.15
4.20	4.20
4.25	4.25
4.30	4.30
4.35	4.35
4.40	4.40
4.45	4.45
4.50	4.50
4.55	4.55
4.60	4.60
4.65	4.65
4.70	4.70
4.75	4.75
4.80	4.80
4.85	4.85
4.90	4.90
4.95	4.95
5.00	5.00
5.05	5.05
5.10	5.10
5.15	5.15
5.20	5.20
5.25	5.25
5.30	5.30
5.35	5.35
5.40	5.40
5.45	5.45
5.50	5.50
5.55	5.55
5.60	5.60
5.65	5.65
5.70	5.70
5.75	5.75
5.80	5.80
5.85	5.85
5.90	5.90
5.95	5.95
6.00	6.00
6.05	6.05
6.10	6.10
6.15	6.15
6.20	6.20
6.25	6.25
6.30	6.30
6.35	6.35
6.40	6.40
6.45	6.45
6.50	6.50
6.55	6.55
6.60	6.60
6.65	6.65
6.70	6.70
6.75	6.75
6.80	6.80
6.85	6.85
6.90	6.90
6.95	6.95
7.00	7.00
7.05	7.05
7.10	7.10
7.15	7.15
7.20	7.20
7.25	7.25
7.30	7.30
7.35	7.35
7.40	7.40
7.45	7.45

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Technical Services, Inc.
International Relations
Division

COMMENTS:

Bag # 203

FIELD DATA - CRITICAL ORIFICE

PLANT CCSD-Stack #2 RUN No. #2 AMBIENT TEMP. (°F) 65
 LOCATION Unit 2 Stack CONTAMINANTS Benzene/Vinyl Chloride BARO. PRESS. (in. Hg) 30.08
 DATE 4/10/90 OPERATOR MB

CALIBRATION DATA

CALIBRATION RUN No.	BURETTE VOL. (cc)	ORIFICE TEMP. (°F)	TIME (sec)
PRE-TEST-1			
2			
3			
Avg.			

FLOW (L/min)

POST-TEST-1			
2			
3			
Avg.			

FLOW (L/min)

Average Flow (L/min)	
----------------------	--

TEST DATA

CLOCK TIME	SAMPLING TIME (min)	FLOWMETER RDG.	ORIFICE TEMP (°F)
Start 2:57			
Stop 2:47			
Total			
			Avg.

COMMENTS: Bag # 204
Galsen
 Technical Services, Inc.
 Environmental Sciences Division

FIELD DATA – CRITICAL ORIFICE

PLANT CCSD RUN No. #313 AMBIENT TEMP. (°F) 65
LOCATION Ditch 2 South CONTAMINANTS Benzene BARO. PRESS. (In. Hg) 30.08
DATE 4/10/80 OPERATOR ML

CALIBRATION DATA

SALINATION RUN No.	BURETTE VOL. (cc)	ORIFICE TEMP. (°F)	TIME (sec)
PRE-TEST - 1			
2			
3			
Avg.			

FLOOR (Landing)

POST-TEST-1			
2			
3			
Avy.			

FLOW (L/min):

Average Flow (l/min)	
10	10
20	20
30	30
40	40
50	50
60	60
70	70
80	80
90	90
100	100
110	110
120	120
130	130
140	140
150	150
160	160
170	170
180	180
190	190
200	200
210	210
220	220
230	230
240	240
250	250
260	260
270	270
280	280
290	290
300	300
310	310
320	320
330	330
340	340
350	350
360	360
370	370
380	380
390	390
400	400
410	410
420	420
430	430
440	440
450	450
460	460
470	470
480	480
490	490
500	500
510	510
520	520
530	530
540	540
550	550
560	560
570	570
580	580
590	590
600	600
610	610
620	620
630	630
640	640
650	650
660	660
670	670
680	680
690	690
700	700
710	710
720	720
730	730
740	740
750	750
760	760
770	770
780	780
790	790
800	800
810	810
820	820
830	830
840	840
850	850
860	860
870	870
880	880
890	890
900	900
910	910
920	920
930	930
940	940
950	950
960	960
970	970
980	980
990	990
1000	1000

TEST DATA

CLOCK TIME	SAMPLING TIME (min)	FLOWMETER RDG.	ORIFICE TEMP (°F)
4:53			
5:30			
Total			Avg.

Start → Stop

Gabson

Technical Services, Inc.
Environmental Sciences
Division

COMMENTS:

Blank #209 (Filed w/ #3)

Particulate and Metals (11) Emission Data

SUMMARY OF TEST DATA - PARTICULATE AND METALS EMISSIONS

PLANT: CCCSD

STACK #: INCINERATOR #2

	<u>RUN #4</u>	<u>RUN #5</u>	<u>RUN #6</u>
NUMBER OF SAMPLING POINTS	24	24	24
DURATION OF THE RUN, MINUTES	120	120	120
SAMPLING NOZZLE DIAMETER, INCHES	0.268	0.268	0.268
PITOT CALIBRATION FACTOR (CF)	0.84	0.84	0.84
METER CALIBRATION FACTOR, GAMMA	1.006	1.006	1.006
STACK DIAMETER, INCHES	41	41	41
AMBIENT AIR TEMPERATURE, °F	65	70	60
BAROMETRIC PRESSURE, INCHES HG	30.14	30.14	30.11
AVG STATIC PRES IN FLUE, INCHES H ₂ O	-0.20	-0.13	-0.13
ABSOLUTE PRES IN FLUE (P(S)), INCHES HG	30.13	30.13	30.10
AVG STACK VELOCITY HEAD, SQRT(ΔP)	0.673	0.696	0.703
AVERAGE ORIFICE (ΔH), INCHES H ₂ O	2.11	2.28	2.35
VOL SAMPLED (V(M)), FT ³ (METER COND)	95.96	100.09	99.91
AVERAGE STACK TEMPERATURE (T(S)), °F	154	153	142
AVERAGE IMPINGER OUTLET TEMP, °F	60	65	68
AVERAGE METER TEMPERATURE, °F	84	88	95
AVERAGE METER VACUUM, INCHES Hg	5.1	4.6	8.7
VOLUME OF WATER CONDENSED (V(LC)), ML	39.5	44.4	43.0
SPECIFIC GRAVITY OF FLUE GAS (SG)	1.011	1.010	1.008
WEIGHT COLLECTED:			
• AHEAD OF FILTER, GMS	0.0113	0.0079	0.0015
• <u>ON THE FILTER, GMS</u>	<u>0.0152</u>	<u>0.0183</u>	<u>0.0217</u>
• TOTAL, GMS	0.0265	0.0262	0.0232
ORSAT ANALYSIS:			
• % CO ₂	5.7	5.8	5.2
• % O ₂	14.3	14.0	14.8
• % CO	0.0	0.0	0.0

SUMMARY OF TEST DATA - PARTICULATE AND METALS EMISSIONS

PLANT: CCCSD

STACK #: INCINERATOR #2

	<u>RUN #4</u>	<u>RUN #5</u>	<u>RUN #6</u>
A. AREA OF STACK, FT ²	9.17	9.17	9.17
B. VOLUME SAMPLED (METER COND.), FT ³	95.96	100.09	99.91
C. VOLUME SAMPLED (STANDARD COND.), SCF $\frac{B \cdot \text{GAMMA} \cdot [P(\text{BAR}) + (\Delta H / 13.6)] \cdot 530}{(29.92) \cdot [T(M)]}$	95.22	98.62	97.19
D. VOLUME OF LIQUID WATER CONDENSED, ML	39.5	44.4	43.0
E. VAPOR VOLUME OF WATER CONDENSED, SCF (STD. CONDITIONS), D=0.04728	1.87	2.10	2.03
F. MOISTURE, %, $(E/(E+C)) \cdot 100$	1.92	2.08	2.05
G. AVERAGE VELOCITY IN THE STACK, FPM $\frac{4005 \cdot (\text{SQRT}(\Delta P) \cdot \text{CF} \cdot \text{SQRT}((TS \cdot 29.92 \cdot 1.0)/(530 \cdot P(S) \cdot SG)))}{\text{A} \cdot G}$	2,415	2,497	2,503
H. STACK GAS FLOW RATE (STACK COND.), CFM A * G	22,140	22,898	22,945
I. STACK GAS FLOW RATE (STD. COND., DRY), DSCFM $H \cdot (1 - (F/100)) \cdot (530/T(S)) \cdot (P(S)/29.92)$	18,886	19,506	19,906
J. TOTAL PARTICULATE COLLECTED, GMS	0.0265	0.0262	0.0232
K. PARTICULATE CONCENTRATION, GRAINS/DSCF $(J \cdot 15.43)/C$	0.0043	0.0041	0.0037
L. PARTICULATE EMISSION RATE, LBS/HR $(K \cdot 1 \cdot 60)/7000$	0.69	0.69	0.63
M. SLUDGE FEED RATE, TONS (DRY)/HR	1.7	1.6	1.5
N. PARTICULATE EMISSION RATIO, LBS/TON-DRY L / M	0.41	0.43	0.42

SUMMARY OF TEST DATA - PARTICULATE AND METALS EMISSIONS

PLANT: CCCSD

STACK #: INCINERATOR #2

	RUN #4	RUN #5	RUN #6
O. QUANTITY COLLECTED ¹ , MG			
Arsenic	0.015	0.009	0.012
Beryllium	< 0.002	< 0.002	< 0.002
Cadmium	0.021	0.029	0.032
Chromium (Total)	0.026	0.026	0.041
Copper	0.10	0.12	0.15
Lead	0.048	0.074	0.074
Manganese	0.836	0.224	0.062
Mercury	0.1169	0.1784	0.2853
Nickel	0.006	0.004	< 0.010
Selenium	0.026	0.034	0.036
Zinc	1.75	2.00	9.35

P. METALS CONCENTRATION, MG/DSCM
 (O * 35.3) / C

Arsenic	0.006	0.003	0.004
Beryllium	< 0.001	< 0.001	< 0.001
Cadmium	0.008	0.010	0.012
Chromium (Total)	0.010	0.009	0.015
Copper	0.037	0.043	0.054
Lead	0.018	0.026	0.027
Manganese	0.310	0.080	0.023
Mercury	0.043	0.064	0.104
Nickel	0.002	0.001	< 0.004
Selenium	0.010	0.012	0.013
Zinc	0.648	0.716	3.396

¹ Quantities represent the sum of the front-half (i.e., filter, Containers A and B) and back-half (Container D) sample fractions. Mercury quantities also include the Container E samples. Data are not corrected for blank quantities. Non-detectable quantities represent the sum of the front-half sample detection limits. Refer to the laboratory data presented in Appendix VI for additional detail.

SUMMARY OF TEST DATA - PARTICULATE AND METALS EMISSIONS

PLANT: CCCSD

STACK #: INCINERATOR #2

	RUN #4	RUN #5	RUN #6
Q. METALS EMISSION RATE, GM/HR			
(P*1*60)/(35.3*10³)			
Arsenic	0.18	0.11	0.15
Beryllium	< 0.02	< 0.02	< 0.02
Cadmium	0.25	0.34	0.39
Chromium (Total)	0.31	0.31	0.50
Copper	1.19	1.42	1.84
Lead	0.57	0.88	0.91
Manganese	9.95	2.66	0.76
Mercury	1.39	2.12	3.51
Nickel	0.07	0.05	< 0.12
Selenium	0.31	0.40	0.44
Zinc	20.81	23.73	114.90

R. METALS EMISSION RATIO, GM/TON (DRY)
Q / M

Arsenic	0.10	0.07	0.10
Beryllium	< 0.01	< 0.01	< 0.02
Cadmium	0.15	0.22	0.26
Chromium (Total)	0.18	0.19	0.34
Copper	0.70	0.89	1.23
Lead	0.34	0.55	0.61
Manganese	5.85	1.66	0.51
Mercury	0.82	1.32	2.34
Nickel	0.04	0.03	< 0.08
Selenium	0.18	0.25	0.29
Zinc	12.24	14.83	76.60

ORSAT DATA AND GAS DENSITY CALCULATIONS

PLANT: CCCSD

STACK #: INCINERATOR #2

PARAMETER	RUN #4		RUN #5		RUN #6	
	DRY BASIS	WET BASIS	DRY BASIS	WET BASIS	DRY BASIS	WET BASIS
CO ₂	5.70	5.59	5.80	5.68	5.20	5.09
O ₂	14.30	14.02	14.00	13.71	14.80	14.50
CO	0.0	0.0	0.0	0.0	0.0	0.0
N ₂	80.00	78.45	80.20	78.53	80.00	78.36
H ₂ O	---	1.94	---	2.08	---	2.05
MOLECULAR WEIGHT ¹	---	29.26	---	29.25	---	29.19
SPECIFIC GRAVITY OF GAS ²	---	1.011	---	1.010	---	1.008

¹ Calculated from the equation:

Molecular Weight = $0.44 \cdot (\%CO_2) + 0.32 \cdot (\%O_2) + 0.28 \cdot (\%N_2 + \%CO) + 0.18 \cdot (\%H_2O)$

² SG= Molecular Weight of Stack Gas/ Molecular Weight of Air (28.95 gm/gm-mole)

ISOKINETIC VARIATION CALCULATION

PLANT: CCCSD

STACK #: INCINERATOR #2

PARAMETER	RUN #4	RUN #5	RUN #6
T(S), °R	614	613	602
V(LC), ML	39.5	44.4	43.0
GAMMA	1.006	1.006	1.006
V(M), FT ³	95.96	100.09	99.91
T(M), °R	544	548	555
P(BAR)+(ΔH/13.6), IN HG	30.30	30.31	30.28
V(S), FPM	2,415	2,497	2,503
P(S), IN HG	30.13	30.13	30.10
A(N), FT ²	0.00039	0.00039	0.00039
THETA, MINUTES	120	120	120
I (PERCENT OF ISOKINETIC) ¹	98.4	98.6	95.2

$$^1 I = \frac{(T(S) \cdot 100((0.00267 \cdot V(CL)) + (V(M)/T(M)) \cdot GAMMA \cdot (P(BAR) + (\Delta H/13.6))))}{(THETA \cdot V(S) \cdot P(S) \cdot A(N))}$$

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Galson
Technical Services

Comments:

100 / 0.37
T=150 / C=0.40

SAMPLE COLLECTION DATA

Plant CRSD
 Location Unit 2 - Stack
 Date 4/11/98
 Run Number 24 - HM
 Operator RR/ML
 Sample Box ID 005
 Meter Box ID 4077
 Probe ID
 Filter #

Meter 1.006
 Meter ΔH₀ 1.72
 Pilot C.F. 0.84
 Assumed Moisture % 4
 Nozzle Diameter in. 0.268
 C Factor 0.40
 Ambient Temperature 65
 Barometric Pressure 30.4
 Silica Gel #

Static Pressure:
 Traverse Pt. 85
 Pwake -0.34
 Pstatic

Water Collected:
 Impingers, ml. 212 + 102 = 314
 Silica Gel, gms. 25.5

318.78 0.62 + 408

Traverse Point Number	Sampling Time min.	Stack Temp. (Ts) °F	Stack ΔP in. H ₂ O	Orifice ΔH in. H ₂ O	Meter Reading (V _m) ft ³	Dry Gas Meter Temp.		Sample Box Temp. °F	Probe Temp. °F	Impinger Outlet °F	Pump Vac. in Hg.
						T in °F	T out °F				
EP2	5	175	0.51	2.35	333.1	69	74	227	235	60	5.5
11	10	176	0.51	2.35	327.3	73	74	262	225	58	5
10	15	176	0.53	2.45	331.4	82	75	248	230	55	5.5
19	20	175	0.48	2.35	335.5	83	76	233	234	56	5.5
* 8	25	164	0.51	2.35	339.7	84	76	246	240	58	5.5
7	30	164	0.49	2.25	—	86	77	238	268	58	5.5
6	35	134	0.38	1.75	347.5	87	78	252	241	59	5
5	40	130	0.36	1.65	351.1	87	79	246	231	59	4.5
4	45	130	0.34	1.55	354.6	89	80	244	225	60	4
3	50	133	0.35	1.60	358.1	88	81	247	224	58	4
12	55	132	0.33	1.50	361.5	89	81	268	243	59	4
1	60	124	0.24	1.10	364.56	89	82	254	238	60	3.5
Averages											

Sp: 27



Galson
Technical Services

Comments:

SAMPLE COLLECTION DATA

Plant CCSD
Location Unit 2 - Stack
Date 4/1/89
Run Number 147-HM
Operator THZ
Sample Box ID 005
Meter Box ID 005
Probe ID 137
Filter # 364.564

Meter Ø _____
Meter ΔH@ _____
Pilot C.F. _____
Assumed Moisture % _____
Nozzle Diameter in. _____
C Factor _____
Ambient Temperature _____
Barometric Pressure _____
Silica Gel # _____

Static Pressure:

Traverse Pt. A-4 A-1
Pwake -0.36 -0.31
Pstatic _____

Water Collected:

Inpingers, ml. _____
Silica Gel, gms. _____

Traverse Point Number	Sampling Time min.	Stack Temp. (Ts) °F	Stack ΔP in. H2O	Orifice ΔH in. H2O	Meter Reading (V _m) ft3	Dry Gas Meter Temp.		Sample Box Temp. °F	Probe Temp. °F	Impinger Outlet °F	Pump Vac. in Hg.
						T in °F	T out °F				
1	65	149	0.46	2.10	368.7	76	80	237	229	64	5
2	70	150	0.48	2.20		83	80	236	240	63	5
3	75	148	0.49	2.25	376.8	87	81	258	240	59	5.5
4	80	151	0.50	2.30	381.0	90	82	276	235	58	5.5
5	85	151	0.52	2.40	385.3	93	83	256	236	58	5.5
6	90	153	0.55	2.55	387.7	93	84	241	238	55	6
7	95	162	0.54	2.50	394.2	92	84	235	237	58	5.5
8	100	171	0.52	2.40	398.4	96	85	234	243	63	5.5
9	105	173	0.50	2.30	402.7	95	86	232	248	64	5.5
10	110	176	0.51	2.35	-	96	87	231	246	66	5.5
11	115	172	0.51	2.35	411.1	95	87	230	244	65	5.5
12	120	116	0.37	1.70	414.74	94	87	231	244	66	4.5
Averages		153.54	0.673	2.11	95.96	84.06		244.25	238.08	59.96	5.08



Galson
Technical Services

Comments:

100 / 0.37
150 / 0.40

SAMPLE COLLECTION DATA

Plant CCSD
Location Unit 2
Date 4/11/90
Run Number 5 Metals
Operator DR
Sample Box ID 013-2
Meter Box ID 005
Probe ID 4
Filter # 415.029

Meter 1.006
Meter ΔH @ 1.72
Pilot C.F. 0.84
Assumed Moisture % 5
Nozzle Diameter in. 0.268
C Factor 0.40
Ambient Temperature 70
Barometric Pressure 30.14
Silica Gel # 4

Static Pressure:

Traverse Pt. 14

Pwake -0.33

Pstatic

Water Collected:

208 + 103 = 311 - 300
Impingers, ml. 114.11

Silica Gel, grms. 33.4
0.5 - 14.4

Traverse Point Number	Sampling Time min.	Stack Temp. (Ts) °F	Stack ΔP in. H ₂ O	Orifice ΔH in. H ₂ O	Meter Reading (V _m) ft ³	Dry Gas Meter Temp.		Sample Box Temp. °F	Probe Temp. °F	Impinger Outlet °F	Pump Vac. in Hg.
						T in °F	T out °F				
A12	5	146	0.55	2.55	419.6	76	81	227	242	74	5
11	10	150	0.66	3.10	424.4	84	82	228	227	76	6
10	15	150	0.62	2.85	429.2	90	83	233	226	64	6
9	20	148	0.54	2.50	433.4	91	84	264	234	59	5
8	25	148	0.56	2.60	437.8	93	84	252	240	58	5
7	30	151	0.57	2.60	-	94	86	246	242	58	5
6	35	159	0.53	2.55	-	96	87	242	243	61	5
5	40	163	0.54	2.50	451.1	98	87	244	246	64	5
4	45	163	0.53	2.4	453.1	100	88	241	250	64	5
3	50	164	0.55	2.55	456.9	96	88	243	249	63	5
2	55	168	0.50	2.30	461.4	96	89	243	240	65	4
1	60	164	0.48	2.25	468.12	93	89	240	231	64	4
Averages											

Start
5:10
2:10

Stop
5:40
3:10

3/2



Comments:
Post-Test
Leak Rate = 0.006 CFM
@ 8" Hg.

SAMPLE COLLECTION DATA

Plant	Location	Date	Run Number	Operator	Sample Box ID	Meter Box ID	Probe ID	Filter #
CCCSD	Unit # 2, Skid	4/11/90	135-AM			005		137
Meter Ø	Meter Δ H@	Pilot C.F.	Assumed Moisture %	Nozzle Diameter in.	C Factor	Ambient Temperature	Barometric Pressure	Silica Gel #
Static Pressure:	Traverse Pt. B3	Pwake 1117	Pstatic	Water Collected:	Inpingers, ml.	Silica Gel, gms.		

Traverse Point Number	Sampling Time min.	Stack Temp. (Ts) °F	Stack ΔP in. H2O	Orifice ΔH in. H2O	Meter Reading (V _m) ft3	Dry Gas Meter Temp.		Sample Box Temp. °F	Probe Temp. °F	Impinger Outlet °F	Pump Vac. in Hg.
						T in °F	T out °F				
B12	5	177	0.65	3.00		81	86	232	216	72	5.5
11	10	176	0.56	2.60	470.8	90	86	234	224	67	5
10	15	177	0.58	2.70	479	92	86	232	236	66	5.0
9	20	173	0.52	2.41	483.1	91	86	231	235	64	5
8	25	174	0.5	2.34	487.6	90	86	230	233	64	5
7	30	168	0.48	2.25	491.7	90	86	235	233	64	4.5
6	35	137	0.39	1.80	496.2	90	86	226	231	63	3.75
5	40	130	0.35	1.64	499.3	89	86	226	229	63	3.75
4	45	125	0.32	1.50	503.3	88	85	233	228	66	3.5
3	50	124	0.31	1.45	506.2	89	86	234	230	66	3.2
2	55	125	0.29	1.35	509.9	88	86	235	230	66	3.0
1	60	123	0.22	1.03	513.1	88	85	231	230	66	2.8
STOP @ 4:21 pm				V _f = 515.14							
Averages		153.46	0.696	2.28	100.09		88.15	236.88	234.58	64.88	4.6

GRIFFIN 1/2 SAMPLE COLLECTION DATA

Technical Services, Inc.

Plant CCCSO
 Location Unit 2 Stack
 Date 4/2/90
 Run Number #46 - HM
 Operator TH
 Sample Box ID 005
 Meter Box ID 005
 Probe ID 005
 Filter # 005

Static Pressure:

 Traverse # 186

 Probe 0.29

Pellets

Motor 1006
 Meter ΔH_Q 1.77
 Pilot C.F. 0.84
 Assumed Moisture % 14
 Nozzle Diameter In. 0.268
 C Factor 0.40
 Ambient Temperature 60
 Barometric Pressure 30.11
 Silica Gel #

Injurers, int.

1024219

Silica Gel gms.

43

Orsat - Day #

CO2 5.2

O2 14.8

CO

Traverse Point Number	Sampling Time min.	Stack Temp. (Is) °F	Stack ΔP in. H ₂ O	Orifice ΔH in. H ₂ O	Meter Reading (Vin) H ₂ O	Dry Gas Meter Temp. T _{in} °F	T _{out} °F	Sample Box Temp. °F	Probe Temp. °F	Injurer Outlet °F	Injurer Vac. in Hg.
1	5	150	0.72	3.35	520.5	62	66	231	239	59	12
2	10	153	0.72	3.35	526.5	75	68	234	217	65	12
3	15	154	0.65	3.05	531.2	85	69	238	218	61	12
4	20	153	0.62	2.89	535.6	92	72	242	225	67	11.1
5	25	156	0.61	2.85	540.1	95	74	246	228	61	10.8
6	30	153	0.61	2.85	546.1	99	77	247	228	59	10.6
7	35	131	0.47	2.19	549.2	100	80	248	239	57	8.2
8	40	120	0.40	1.87	553.1	100	81	249	237	60	7
9	45	108	0.38	1.77	556.5	99	83	249	239	62	6.7
10	50	110	0.38	1.65	560.4	100	85	249	240	66	6.2
11	55	120	0.27	1.26	562.0	99	87	251	240	67	4.3
12	60	98	0.21	.95	564.2	99	88	253	248	68	4.0
Averages											

Σ = 43

21

1024219

43

P 2/2



Galson
Technical Services

Comments: Post Test
Leak rate
P. 0.008cfm
@ 12 in Hg

SAMPLE COLLECTION DATA

Plant CCSD
 Location Unit 2 Stack
 Date 4-12-9
 Run Number # 6-MM
 Operator CMT
 Sample Box ID 005
 Meter Box ID 005
 Probe ID
 Filter #

Meter ID
 Meter Δ H@
 Pilot C.F.
 Assumed Moisture %
 Nozzle Diameter in.
 C Factor
 Ambient Temperature
 Barometric Pressure
 Silica Gel #

Static Pressure:
 Traverse Pit # 4
 Pwake 0.28
 Pstatic
 Water Collected:
 Impingers, ml.
 Silica Gel, gms.

U₁ = 564.439 or SAT 102.44

Traverse Point Number	Sampling Time min.	Stack Temp. (Ts) °F	Stack ΔP in. H2O	Orifice ΔH in. H2O	Meter Reading (V _m) ft3	Dry Gas Meter Temp.		Sample Box Temp. °F	Probe Temp. °F	Impinger Outlet °F	Pump Vac. in Hg.
						T in °F	T out °F				
1	5	141	0.42	1.5	566.0	86	88	219	260	72	5.4
2	10	143	0.47	2.19	569.4	95	87	233	234	75	7.8
3	15	140	0.47	2.19	573.4	104	90	243	230	75	7.8
4	20	143	0.50	2.34	577.4	110	93	250	235	76	8.6
5	25	144	0.55	2.58	581.7	112	95	251	235	72	9.2
6	30	148	0.55	2.58	585.9	116	98	250	232	70	9.3
7	35	150	0.56	2.57	590.3	118	100	254	230	69	9.3
8	40	146	0.59	2.35	590.9	120	102	254	230	70	8.8
9	45	162	0.52	2.43	599.2	118	103	258	232	72	8.9
10	50	162	0.53	2.61	603.5	119	104	258	229	82	9.7
11	55	158	0.53	2.69	607.8	121	105	255	228	88	9.9
12	60	159	0.45	2.10	612.3	122	107	256	226	77	8.7
					U ₂ = 615.584						
Averages		142.00	0.703	2.35	99.91		94.75	246.50	233.08	68.53	8.68

static
9.5

*

static
10.5

Hexavalent Chromium Emission Data

SUMMARY OF TEST DATA - HEXAVALENT CHROMIUM EMISSIONS

PLANT: CCCSD

STACK #: INCINERATOR #2 EXHAUST

	<u>RUN#4</u>	<u>RUN#5</u>	<u>RUN#6</u>
	24	24	24
NUMBER OF SAMPLING POINTS			
DURATION OF THE RUN, MINUTES	120	120	120
SAMPLING NOZZLE DIAMETER, INCHES	0.268	0.268	0.268
PITOT CALIBRATION FACTOR (CF)	0.84	0.84	0.84
METER CALIBRATION FACTOR, GAMMA	1.014	1.014	1.014
STACK DIAMETER, INCHES	41	41	41
AMBIENT AIR TEMPERATURE, °F	60	70	60
BAROMETRIC PRESSURE, INCHES HG	30.14	30.14	30.11
AVG STATIC PRES IN FLUE, INCHES H ₂ O	-0.14	-0.13	-0.13
ABSOLUTE PRES IN FLUE (P(S)), INCHES HG	30.13	30.13	30.10
AVG STACK VELOCITY HEAD (SQRT(ΔP))	0.690	0.700	0.719
AVERAGE ORIFICE (ΔH), INCHES H ₂ O	2.36	2.44	2.58
VOL SAMPLED (V(M)), FT ³ (METER COND)	96.63	98.55	102.07
AVERAGE STACK TEMPERATURE (T(S)), °F	157	149	142
AVERAGE IMPINGER OUTLET TEMP, °F	70	79	70
AVERAGE METER TEMPERATURE, °F	91	92	96
AVERAGE METER VACUUM, INCHES HG	6.7	4.0	3.6
VOLUME OF WATER CONDENSED (V(LC)), ML	53.7	46.8	57.1
SPECIFIC GRAVITY OF FLUE GAS (SG)	1.008	1.010	1.006
HEXAVALENT CHROMIUM COLLECTED, μG	<7	<8	<8
ORSAT ANALYSIS:			
%CO ₂	5.7	5.8	5.2
%O ₂	14.3	14.0	14.8
%CO	0.0	0.0	0.0

SAMPLING DATA & CALCULATIONS - HEXAVALENT CHROMIUM EMISSIONS

PLANT: CCCSD

STACK #: INCINERATOR #2 EXHAUST

	RUN#4	RUN#5	RUN#6
A. AREA OF STACK, FT ²	9.17	9.17	9.17
B. VOLUME SAMPLED (METER COND.), FT ³	96.63	98.55	102.07
C. VOLUME SAMPLED (STANDARD COND.), FT ³ $\frac{B \cdot \text{GAMMA} \cdot P(\text{BAR}) + (\Delta H / 13.6) \cdot 530}{[(29.92) \cdot T(M)]}$	95.52	97.25	99.86
D. VOLUME OF LIQUID WATER CONDENSED, ML	53.7	46.8	57.1
E. VAPOR VOLUME OF WATER CONDENSED, SCF (STD. CONDITIONS), $D \cdot 0.04728$	2.54	2.21	2.70
F. MOISTURE, %, $(E/(E+C)) \cdot 100$	2.59	2.22	2.63
G. AVERAGE VELOCITY IN THE STACK, FPM $\frac{4005 \cdot (\text{SQRT}(\Delta P)) \cdot \text{CF} \cdot \text{SQRT}((T(S) \cdot 29.92 \cdot 1.0) / (530 \cdot P(S) \cdot \text{SG}))}{\text{SQRT}((T(S) \cdot 29.92 \cdot 1.0) / (530 \cdot P(S) \cdot \text{SG}))}$	2,486	2,504	2,563
H. STACK GAS FLOW RATE (STACK COND.), CFM $A \cdot G$	22,793	22,960	23,497
J. STACK GAS FLOW RATE (STANDARD CONDITIONS, DRY STATE), DSCFM $H \cdot (1 - (F/100)) \cdot (530/T(S)) \cdot (P(S)/29.92)$	19,201	19,660	20,259
K. HEXAVALENT CHROMIUM COLLECTED, μg	< 7	< 8	< 8
L. HEXAVALENT CHROMIUM CONC., $\mu\text{g/DSCM}$ $(K/C) \cdot 35.3$	< 3	< 3	< 3
M. HEXAVALENT CHROMIUM EMISSION RATE, GM/HR $[(L \cdot J \cdot 60) \cdot 10^{-6}] / 35.3$	< 0.1	< 0.1	< 0.1
N. SLUDGE FEED RATE, TONS/HR (DRY)	1.7	1.6	1.5
O. HEXAVALENT CHROMIUM EMISSION RATIO, GM/TON M / N	< 0.05	< 0.06	< 0.06

ORSAT DATA AND GAS DENSITY CALCULATIONS

PLANT: CCCCSD

STACK #: INCINERATOR #2 EXHAUST

PARAMETER	RUN #4		RUN #5		RUN #6	
	DRY BASIS	WET BASIS	DRY BASIS	WET BASIS	DRY BASIS	WET BASIS
CO ₂	5.70	5.55	5.80	5.67	5.20	5.06
O ₂	14.30	13.93	14.00	13.69	14.80	14.41
CO	0	0	0	0	0	0
N ₂	80.00	77.93	80.20	78.42	80.00	77.89
H ₂ O	- -	2.59	- -	2.22	- -	2.63
MOLECULAR WEIGHT ¹	- -	29.19	- -	29.23	- -	29.12
SPECIFIC GRAVITY OF GAS ²	- -	1.008	- -	1.010	- -	1.006

¹ CALCULATED FROM THE EQUATION:

MOLECULAR WEIGHT = $0.44(\%CO_2) + 0.32(\%O_2) + 0.28(\%N_2 + \%CO) + 0.18(\%H_2O)$

² SG = MOLECULAR WEIGHT STACK GAS / MOLECULAR WEIGHT OF AIR (28.95 GM/MOLE)

ISOKINETIC VARIATION CALCULATION

PLANT: CCCSD

STACK #: INCINERATOR #2 EXHAUST

PARAMETER	RUN #4	RUN #5	RUN #6
T(S), °R	617	609	602
V(LC), ML	53.7	46.8	57.1
GAMMA	1.014	1.014	1.014
V(M), FT ³	96.63	98.55	102.07
T(M), °R	551	552	556
P(BAR)+(ΔH/13.6), IN HG	30.31	30.32	30.30
V(S), FPM	2,486	2,504	2,563
P(S), IN HG	30.13	30.13	30.10
A(N), FT ²	0.00039	0.00039	0.00039
THETA, MINUTES	120	120	120
I (PERCENT OF ISOKINETIC)	97.0	96.5	96.1

$$I = \frac{(T(S)(AVG) \cdot 100((0.00267 \cdot V(CL)) + (V(M)/T(M)) \cdot GAMMA \cdot (P(BAR) + (\Delta H/13.6))))}{(THETA \cdot V(S) \cdot P(S) \cdot A(N))}$$

APPENDIX VI: LABORATORY DATA

HCI Data



6601 Kirkville Road
E. Syracuse, NY 13057
Tel: (315) 432-0506
1-800-950-0506

LABORATORY ANALYSIS REPORT

Client: COOSD
Task Number: 90042315
Location: NS

Job Number: SE034LL
Date Sampled: 04/10-12/90

HYDROCHLORIC ACID STACK

Sample ID	Lab ID	SAMPLE VOL (ML)	CHLORIDE CONC. (MG/L)	BLANK-CORRECTED CONC. (MG/L)	TOTAL CHLORIDE (MG)	TOTAL(1) HCL (MG)
TEST 1	J9301	255	1.9	1.5	0.38	0.39
TEST 2	J9302	295	1.9	1.5	0.45	0.46
TEST 3	J9303	275	2.2	1.8	0.50	0.51
BLANK	J9304BL	215	0.4	NA	NA	NA

(<) - Less Than
(>) - Greater Than
NA - Not Applicable
ND - Not detectable
NS - Not specified
MG - Milligrams
L - Liters
M3 - Cubic Meter
MG/M3 - Milligrams Per Cubic Meter
PPM - Parts Per Million
UG - Micrograms
NG - Nanograms
G - Grams
WT - Weight

Method(s): CARB 421

Footnotes: (1) TOTAL HCL =
TOTAL CHLORIDE X 36.5
35.5

Submitted by: NSA

Approved by: *[Signature]*

Date: 4-MAY-1990

Formaldehyde, Benzene, and Vinyl Chloride Data



ALPHA CHEMICAL & BIOMEDICAL LABORATORIES

Joe E. Hodgkins, Ph.D.
Director

April 23, 1990

GALSON TECHNICAL SERVICES INC.
Attn: Chuck Siu
2116 Berkeley Way
Berkeley, CA. 94704

**REPORT
FORMALDEHYDE ANALYSIS
PROJECT # SE-034**

Sample Identification:

General Information: DNPH-Formaldehyde samples, see results for individual description.

Received in Lab : 4/11/90 9:25 am. See Chain of Custody.

Analysis:

Formaldehyde by High Performance Liquid Chromatography, CARB Method 430.

Sampling impinger solution preparation date: 4/9/90.

Extraction date: 4/16/90.

Analysis date: 4/20/90.

Instrument : Perkin-Elmer Series 4 HPLC.
Detector : Perkin-Elmer UV @ 360 nm.
Column : Brownlee ODS-224 RP-18 4.6 x 220 mm with ODU guard column.
Mobile phase : 30:70 ACN:H₂O to ACN
Conditions : Linear gradient for 20 min., 5 min. wash.
Flow rate : 2.0 ml/min
Injection size : 25 ul

RECEIVED
APR 25 1990
Galsen Technical Services

GALSON TECHNICAL SERVICES

RE: Project # SE-034

April 23, 1990

Page 2

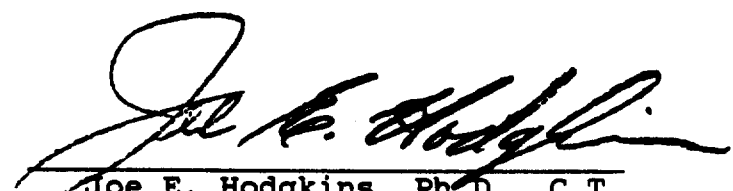
Results:

<u>Sample #</u>	<u>Galson #</u>	<u>Formaldehyde ug*</u>
8482	SE03401	2.59
8483	SE03402	0.85
8484	SE03403	2.00
8485	SE03404 (Blank)	0.77

Method Detection Limit = 0.4 ug

*Results are compensated for the travel blank.


Mark S. Fesler
Analyst


Joe E. Hodgkins, Ph.D., C.T.
Laboratory Director

Enclosure (Chain of Custody)

900405

AIR TOXICS LTD.

SAMPLE NAME: Test #1 Bag 203

ID#: 900405-01A

Stationary Source Test Method - Low Level Benzene/Vinyl Chloride
(CARB Method 410A/422)
Cryofocusing Full Scan GC/MS

File Name: 1041209
Dil. Factor: 3.87

Date of Collection: 4/11/90
Date of Analysis: 4/12/90

	<u>MDL (ppbv)</u>	<u>Amount (ppbv)</u>
Benzene	4.0	ND
Vinyl Chloride	4.0	ND

900405

AIR TOXICS LTD.

SAMPLE NAME: Test #2 Bag 204

ID#: 900405-02A

Stationary Source Test Method - Low Level Benzene/Vinyl Chloride

(CARB Method 410A/422)

Cryofocusing Full Scan GC/MS

File Name: 1041210

Date of Collection: 4/11/90

Dil. Factor: 3.87

Date of Analysis: 4/12/90

	<u>MDL (ppbv)</u>	<u>Amount (ppbv)</u>
Benzene	4.0	ND
Vinyl Chloride	4.0	ND

AIR TOXICS LTD.

SAMPLE NAME: Test #3

ID#: 900405-03A

Stationary Source Test Method - Low Level Benzene/Vinyl Chloride
(CARB Method 410A/422)
Cryofocusing Full Scan GC/MS

File Name: 1041211
Dil. Factor: 2

Date of Collection: 4/11/90
Date of Analysis: 4/12/90

	<u>MDL (ppbv)</u>	<u>Amount (ppbv)</u>
Benzene	1.0	1.0
Vinyl Chloride	1.0	ND

900405

AIR TOXICS LTD.

SAMPLE NAME: Trip Blank

ID#: 900405-04A

Stationary Source Test Method - Low Level Benzene/Vinyl Chloride

(CARB Method 410A/422)

Cryofocusing Full Scan GC/MS

File Name: 1041205

Date of Collection: NA

Dil. Factor: 2

Date of Analysis: 4/12/90

	<u>MDL (ppbv)</u>	<u>Amount (ppbv)</u>
Benzene	ND	ND
Vinyl Chloride	ND	ND

900405

AIR TOXICS LTD.

SAMPLE NAME: Lab Blank

ID#: 900405-05A

Stationary Source Test Method - Low Level Benzene/Vinyl Chloride

(CARB Method 410A/422)

Cryofocusing Full Scan GC/MS

File Name: 1041203

Date of Collection: NA

Dil. Factor: 2

Date of Analysis: 4/12/90

	<u>MDL (ppbv)</u>	<u>Amount (ppbv)</u>
Benzene	1.0	ND
Vinyl Chloride	2.0	ND

900405

AIR TOXICS LTD.

SAMPLE NAME: Method Spike

ID#: 900405-05B

Stationary Source Test Method - Low Level Benzene/Vinyl Chloride

(CARB Method 410A/422)

Cryofocusing Full Scan GC/MS

File Name: 1041202

Date of Collection: NA

Dil. Factor: 2

Date of Analysis: 4/12/90

	<u>MDL (ppbv)</u>	<u>% Recovery</u>
Benzene	2.0	100
Vinyl Chloride	2.0	100

Particulate and Metals (11) Data



Galson Technical Services, Inc.
2116 Berkeley Way
Berkeley, CA 94704
Tel: (415) 848-0389
FAX: (415) 848-0838

PARTICULATE ANALYSIS REPORT - FILTER SAMPLES

Project Name: **COOSD**
Project No.: **SE-034**

Sample ID	Filter ID	Sample Date	Tare (gm)	Final (gm)	Diff. (gm)	Blk-Correct
						Diff. (gm)
Blank	136	4/11/90	0.3703	0.3715	0.0012	NA
Test #4	137	4/11/90	0.3712	0.3876	0.0164	0.0152
Test #5	139	4/11/90	0.3668	0.3863	0.0195	0.0183
Test #6	140	4/12/90	0.3698	0.3927	0.0229	0.0217

Method: **CARB 5**
Date Analyzed: **4/19/90**
Analyzed by: **S. Valladolid**

Approved by: **M. Ludwiczak**



Galson Technical Services, Inc.
2116 Berkeley Way
Berkeley, CA 94704
Tel: (415) 848-0389
FAX: (415) 848-0838

PARTICULATE ANALYSIS REPORT - RINSE SAMPLES

Project Name: CCCSD

Project No.: SE-034

Sample ID	Lab ID	Sample Date	Tare (gm)	Final (gm)	Diff. (gm)	Blk-Correct
						Diff. (gm)
Blank	Z	4/11/90	106.4651	106.4720	0.0069	NA
Test #4	AA	4/11/90	97.7315	97.7497	0.0182	0.0113
Test #5	CC	4/11/90	99.2853	99.3001	0.0148	0.0079
Test #6	FF	4/12/90	100.3998	100.4082	0.0084	0.0015

Method: CARB 5

Date Analyzed: 4/19-20/1990

Analyzed by: S. Valladolid

Approved by: M. Ludwiczak



6601 Kirkville Road
E Syracuse, NY 13057
Tel. (315) 432-0506
1-800-950-0506

LABORATORY ANALYSIS REPORT

Client: CCCSD
Task Number: 90042315
Location: NS

Job Number: SE034LL
Date Sampled: 04/10-12/90

	Lab ID: J9297AC	J9297B	J9297D	
	Client ID: TEST 4	TEST 4	TEST 4	TEST 4
	CONTAINER A/C	CONTAINER B	CONTAINER D	TOTAL
LEAD	TOTAL MG 0.048	<0.04	<0.1	0.048
CADMIUM	0.021	<0.002	<0.005	0.021
CHROMIUM	0.012	<0.004	0.014	0.026
NICKEL	0.006	<0.008	<0.02	0.006
COPPER	0.10	<0.008	<0.02	0.10
ARSENIC	0.009	<0.002	0.006	0.015
ZINC	0.98	0.69	0.079	1.75
MANGANESE	0.016	<0.002	0.82	0.836
SELENIUM	0.023	0.003	<0.006	0.026
BERYLLIUM	<0.001	<0.001	<0.002	<0.002

Method(s): EPA DRAFT METHOD 8/28/89 METHOD EMISSIONS
FROM HAZARDOUS WASTE AND SIMILAR COMBUSTION
PROCESSES.

Footnotes:

- (<) - Less Than
- (>) - Greater Than
- NA - Not Applicable
- ND - Not detectable
- NS - Not specified
- MG - Milligrams
- L - Liters
- M³ - Cubic Meter
- MG/M³ - Milligrams Per Cubic Meter
- PPM - Parts Per Million
- UG - Micrograms
- NG - Nanograms
- BL - Blank

Submitted by: ES, DS, FH

Approved by: *Mary S. Wilkerson*

Date: 4-MAY-1990



6601 Kirkville Road
E Syracuse, NY 13057
Tel: (315) 432-0506
1-800-950-0506

LABORATORY ANALYSIS REPORT

Client: CCCSD
Task Number: 90042315
Location: NS

Job Number: SE034LL
Date Sampled: 04/10-12/90

	Lab ID: J9299AC	J9299B	J9299D		
	Client ID: TEST 6	TEST 6	TEST 6	TEST 6	
	CONTAINER A/C	CONTAINER B	CONTAINER D	TOTAL	
LEAD	TOTAL MG	0.074	<0.05	<0.1	0.074
CADMIUM		0.032	<0.002	<0.006	0.032
CHROMIUM		0.014	0.009	0.018	0.041
NICKEL		<0.005	<0.01	<0.03	<0.010
COPPER		0.15	<0.01	<0.03	0.15
ARSENIC		0.012	<0.002	<0.007	0.012
ZINC		1.1	8.1	0.15	9.35
MANGANESE		0.014	0.006	0.042	0.062
SELENIUM		0.033	0.003	<0.007	0.036
BERYLLIUM		<0.001	<0.001	<0.003	<0.002

Method(s): EPA DRAFT METHOD 8/28/89 METHOD EMISSIONS
FROM HAZARDOUS WASTE AND SIMILAR COMBUSTION
PROCESSES.

Footnotes: NO BLANK CORRECTIONS FOR CONTAINER
B AND D REQUIRED.

(<) - Less Than
(>) - Greater Than
NA - Not Applicable
ND - Not detectable
NS - Not specified
MG - Milligrams
L - Liters
M³ - Cubic Meter
MG/M³ - Milligrams Per Cubic Meter
PPM - Parts Per Million
UG - Micrograms
NG - Nanograms
BL - Blank

Submitted by: ES, DS, PH

Approved by: *Mary E. Wilkerson*

Date: 4-MAY-1990



6601 Kirkville Road
E Syracuse, NY 13057
Tel: (315) 432-0506
1-800-950-0506

LABORATORY ANALYSIS REPORT

Client: COCSD
Task Number: 90042315
Location: NS

Job Number: SE034LL
Date Sampled: 04/10-12/90

	Lab ID: J9298AC	J9298B	J9298D	
	Client ID: TEST 5	TEST 5	TEST 5	TEST 5
	CONTAINER A/C	CONTAINER B	CONTAINER D	TOTAL
LEAD	TOTAL MG 0.074	<0.06	<0.1	0.074
CADMIUM	0.029	<0.003	<0.006	0.029
CHROMIUM	0.007	0.006	0.013	0.026
NICKEL	0.004	<0.1	<0.02	0.004
COPPER	0.12	<0.01	<0.02	0.12
ARSENIC	0.009	<0.003	<0.006	0.009
ZINC	1.7	0.16	0.14	2.00
MANGANESE	0.014	<0.004	0.21	0.224
SELENIUM	0.028	0.006	<0.006	0.034
BERYLLIUM	<0.001	<0.001	<0.002	<0.002

Method(s): EPA DRAFT METHOD 8/28/89 METHOD EMISSIONS
FROM HAZARDOUS WASTE AND SIMILAR COMBUSTION
PROCESSES.

Footnotes:

- (<) - Less Than
- (>) - Greater Than
- NA - Not Applicable
- ND - Not detectable
- NS - Not specified
- MG - Milligrams
- L - Liters
- M³ - Cubic Meter
- MG/M³ - Milligrams Per Cubic Meter
- PPM - Parts Per Million
- UG - Micrograms
- NG - Nanograms
- BL - Blank

Submitted by: ES, DS, PH

Approved by: *Mary E. Withrow*

Date: 4-MAY-1990



6601 Kirkville Road
E Syracuse, NY 13057
Tel: (315) 432-0506
1-800-950-0506

LABORATORY ANALYSIS REPORT

Client: CCCSD
Task Number: 90042315
Location: NS

Job Number: SE034LL
Date Sampled: 04/10-12/90

	Lab ID: J9300ACBL Client ID: BLANK CONTAINER A/C	J9300BBL BLANK CONTAINER B	J9300DBL BLANK CONTAINER D
LEAD	TOTAL MG <0.02	<0.1	<0.03
CADMIUM	<0.001	<0.004	<0.001
CHROMIUM	0.010	<0.01	<0.003
NICKEL	<0.005	<0.02	<0.006
COPPER	<0.005	<0.02	<0.006
ARSENIC	0.002	<0.005	<0.002
ZINC	0.24	<0.03	<0.008
MANGANESE	0.012	<0.006	<0.002
SELENIUM	0.003	<0.005	<0.002
BERYLLIUM	<0.001	<0.002	<0.001

Method(s): EPA DRAFT METHOD 8/28/89 METHOD EMISSIONS
FROM HAZARDOUS WASTE AND SIMILAR COMBUSTION
PROCESSES.

Footnotes:

- (<) - Less Than
- (>) - Greater Than
- NA - Not Applicable
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- M³ - Cubic Meter
- MG/M³ - Milligrams Per Cubic Meter
- PPM - Parts Per Million
- UG - Micrograms
- NG - Nanograms
- BL - Blank

Submitted by: ES, DS, PH

Approved by: *Mary E. Withron*

Date: 4-MAY-1990



6601 Kirkville Road
E. Syracuse, NY 13057
Tel: (315) 432-0506
1-800-950-0506

LABORATORY ANALYSIS REPORT

Client: CCCSD
Task Number: 90042315
Location: NS

Job Number: SE034LL
Date Sampled: 04/10-12/90

	Lab ID: J9297AC Client ID: TEST 4 CONTAINER A/C	J9297B TEST 4 CONTAINER B	J9297D TEST 4 CONTAINER D	J9297E TEST 4 CONTAINER E	TEST 4 TOTAL
MERCURY TOTAL UG	2.6	0.3	21	93	116.9

Method(s): EPA DRAFT METHOD 8/28/89 METHOD EMISSIONS
FROM HAZARDOUS WASTE AND SIMILAR COMBUSTION
PROCESSES.

Footnotes: NO BLANK CORRECTIONS NEEDED.

(<) - Less Than
(>) - Greater Than
NA - Not Applicable
ND - Not detectable
NS - Not specified
MG - Milligrams
L - Liters
M³ - Cubic Meter
MG/M³ - Milligrams Per Cubic Meter
PPM - Parts Per Million
UG - Micrograms
NG - Nanograms
BL - Blank

Submitted by: PH

Approved by: *Mary Girthrow*

Date: 4-MAY-1990



6601 Kirkville Road
E Syracuse, NY 13057
Tel: (315) 432-0506
1-800-950-0506

LABORATORY ANALYSIS REPORT

Client: CCCSD
Task Number: 90042315
Location: NS

Job Number: SE034LL
Date Sampled: 04/10-12/90

	Lab ID: J9298AC	J9298B	J9298D	J9298E	
	Client ID: TEST 5	TEST 5	TEST 5	TEST 5	TEST 5
	CONTAINER A/C	CONTAINER B	CONTAINER D	CONTAINER E	TOTAL
MERCURY	1.8	0.60	16	160	178.4
TOTAL UG					

Method(s): EPA DRAFT METHOD 8/28/89 METHOD EMISSIONS
FROM HAZARDOUS WASTE AND SIMILAR COMBUSTION
PROCESSES.

Footnotes: NO BLANK CORRECTIONS NEEDED.

(<) - Less Than
(>) - Greater Than
NA - Not Applicable
ND - Not detectable
NS - Not specified
MG - Milligrams
L - Liters
M³ - Cubic Meter
MG/M³ - Milligrams Per Cubic Meter
PPM - Parts Per Million
UG - Micrograms
NG - Nanograms
BL - Blank

Submitted by: ES, DS, PH

Approved by: *Mary E. Wirthon*

Date: 4-MAY-1990



6601 Kirkville Road
E Syracuse, NY 13057
Tel. (315) 432-0506
1-800-950-0506

LABORATORY ANALYSIS REPORT

Client: COCSD
Task Number: 90042315
Location: NS

Job Number: SE034LL
Date Sampled: 04/10-12/90

	Lab ID: J9299AC	J9299B	J9299D	J9299E		
	Client ID: TEST 6	TEST 6	TEST 6	TEST 6	TEST 6	
	CONTAINER A/C	CONTAINER B	CONTAINER D	CONTAINER E	TOTAL	
MERCURY	TOTAL UG	<0.8	1.3	24	260	285.3

Method(s): EPA DRAFT METHOD 8/28/89 METHOD EMISSIONS
FROM HAZARDOUS WASTE AND SIMILAR COMBUSTION
PROCESSES.

Footnotes: NO BLANK CORRECTIONS NEEDED.

(<) - Less Than
(>) - Greater Than
NA - Not Applicable
ND - Not detectable
NS - Not specified
MG - Milligrams
L - Liters
M³ - Cubic Meter
MG/M³ - Milligrams Per Cubic Meter
PPM - Parts Per Million
UG - Micrograms
NG - Nanograms
BL - Blank

Submitted by: ES, DS, PH

Approved by: *Mary E. Irthron*
Date: 4-MAY-1990



Galson Technical Services, Inc.
2116 Berkeley Way
Berkeley, CA 94704
Tel: (415) 848-0389
FAX: (415) 848-0838

SILICA GEL ANALYSIS REPORT

Project Name: **CCSD**
Project No.: **SE-034**

Sample ID	Lab ID	Sample Date	Tare (gm)	Final (gm)	Diff. (gm)	Blk-Correct
						Diff. (gm)
Blank	1219	4/12/90	200.0	200.6	0.6	NA
1-HCl	1214	4/10/90	200.0	213.7	13.7	13.1
2-HCl	1210	4/10/90	200.0	210.2	10.2	9.6
3-HCl	1215	4/10/90	200.0	207.7	7.7	7.1
4-Hex Chrome	1207	4/11/90	200.0	230.3	30.3	29.7
5-Hex Chrome	1202	4/11/90	200.0	224.4	24.4	23.8
6-Hex Chrome	1209	4/12/90	200.0	225.7	25.7	25.1
4-Multi-Metals	1216	4/11/90	200.0	226.1	26.1	25.5
5-Multi-Metals	1198	4/11/90	200.0	234.0	34.0	33.4
6-Multi-Metals	1217	4/12/90	200.0	222.6	22.6	22.0
7-PAH	1221	4/12/90	200.0	234.6	34.6	34.0
8-PAH	1227	4/12/90	300.0	333.9	33.9	33.3
9-PAH	1211	4/13/90	200.0	235.7	35.7	35.1
10-PAH	1218	4/13/90	200.0	235.9	35.9	35.3

Method: **CARB 5**
Date Analyzed: **4/16/90**
Analyzed by: **S. Valladolid**

Approved by: **M. Ludwiczak**



104 / 0.34
150 / 0.37

SAMPLE COLLECTION DATA

Plant CCSD Location Dist 2 - Stock
 Date 4/11/90 Run Number 11 # 45 HC
 Operator RR/7m Sample Box ID WT-SP
 Meter Box ID 004 Probe ID _____
 Filter # _____

VI: 953-605

CO2-5.7 / O2-14.3

Static Pressure:

Traverse Pl. *1/5

Pwaka -0.32

Plastic

Water Collected: 1

Engineers, Inc.

Silica Gel, qms.

[illegible]

CONTINUING:

Post Test
LK Rate Change
@ 10 min

CAISON
Technical Services, Inc.

SAMPLE COLLECTION DATA

Plant CCCSO 2/2
Location Unit 2 Stack
Date 4/12/90
Run Number 6 HEACH
Operator DKRP
Sample Box ID SEP. box
Meter Box ID 004
Probe ID _____
Filter # _____

Static Pressure: _____

Traverse Pt. _____

Pwake _____

Pelate _____

Instruments, ind. _____

Silica Gel, gms. _____

Orsat - Day # _____

CO₂ _____O₂ _____

CO _____

Motor 1.014Meter ΔH @ 1.87Pilot C.F. 0.84Assumed Moisture % 5Nozzle Diameter in. 0.268C Factor 0.375Ambient Temperature 60Barometric Pressure 30.11

Silica Gel # _____

Orsat # 102

Traverse Point Number	Sampling Time min.	Stack Temp. (T _s) °F	Stack ΔP in. H ₂ O	Orifice ΔH in. H ₂ O	Meter Reading (V _m) ft ³	Dry Gas Meter Temp.		Sample Box Temp. °F	Probe Temp. °F	Inlet Outlet °F	Pump Vac. in. Hg.
						T _{in} °F	T _{out} °F				
1	5	111	0.25	1.25	—	83	86	—	262	74	2
2	10	118	0.37	1.85	211.6	95	86	—	249	71	2
3	15	121	0.37	1.85	215.3	105	86	—	243	72	2
4	20	116	0.37	1.85	—	110	90	—	233	75	2
5	25	122	0.39	1.90	222.7	114	92	—	237	—	2
6	30	132	0.46	2.25	226.8	117	94	—	237	76	2
7	35	147	0.47	2.35	231.0	120	96	—	237	76	2
8	40	157	0.80	2.45	235.1	124	101	—	244	—	—
9	45	163	0.55	2.70	239.5	124	102	—	245	77	2
10	50	164	0.58	2.85	—	129	104	—	228	79	2
11	55	160	0.58	2.85	248.5	130	108	—	203	—	5
12	60	161	0.55	2.70	252.872	130	108	—	229	80	5
Averages		140.13	0.719	2.58	102.07			N/A	242.83	69.67	3.63



100 0.34
150 0.375

SAMPLE COLLECTION DATA

Static Pressure:

Traverse P184 *13.1
Pwake -0.22 -0.30

Plastic

Water Collected:

118 + 105 = 223
Impingers, ml.

Silica Gel, am.

Meter Ø - 1.014
Meter ΔH@ 1.87
Pilot C.F. 0.89
Assumed Moisture % 5
Nozzle Diameter in. 0.368
C Factor 0.375
Ambient Temperature 70
Barometric Pressure 30.14
Silica Gel # _____

DESIGN

$$\frac{CO_2 - 5.8}{O_2 - 14.0}$$
$$y = 51362$$
[illegible]



Comments:
Post test Lt rate
0.05 cfm
10 in Hg

SAMPLE COLLECTION DATA

Plant CCCSO 272
Location Unit 2 Stack
Date 4/11/90
Run Number 57 HESCN
Operator DR/AP
Sample Box ID SC2BOX
Meter Box ID FOA
Probe ID _____
Filter # _____

Meter ID 1014
Meter ΔH @ 1.87
Pilot C.F. 0.34
Assumed Moisture % _____
Nozzle Diameter in. 5.268
C Factor 0.375
Ambient Temperature 70
Barometric Pressure _____
Silica Gel # _____

Static Pressure:

Traverse Pt. _____
Pwake _____
Pstatic _____

Water Collected:

Impingers, ml. _____
Silica Gel, gms. _____

Orsat # 06

Traverse Point Number	Sampling Time min.	Stack Temp. (Ts) °F	Stack ΔP in. H2O	Orifice ΔH in. H2O	Meter Reading (Vm) ft3	Dry Gas Meter Temp.		Sample Box Temp. °F	Probe Temp. °F	Impinger Outlet °F	Pump Vac. in Hg.
						T in °F	T out °F				
1	65	165	0.62	3.05	—	82	85	2	256	80	4
2	70	165	0.60	2.95	107.5	94	85	—	236	80	4
3	75	168	0.60	2.95	—	96	85	—	214	80	4
4	80	170	0.58	2.85	—	98	85	—	233	80	4
5	85	167	0.56	2.75	120.8	99	85	—	231	—	4
6	90	164	0.54	2.65	125.0	100	86	—	238	80	4
7	95	155	0.54	2.65	129.2	100	86	—	250	80	4
8	100	152	0.54	2.65	—	99	86	—	245	80	4
9	105	152	0.52	2.55	137.7	100	86	—	245	77	4
10	110	147	0.50	2.45	141.9	101	87	—	256	77	4
11	115	148	0.47	2.30	145.9	101	87	—	264	77	4
12	120	149	0.45	2.20	149.9	100	87	—	278	77	3.5
Averages		149.46	0.700	2.44	98.55	91.85		N/A	245.5	78.55	3.96



Galson
Technical Services

Comments: Post test leak
rate 0.014cfm
@ 17.1 in Hg

SAMPLE COLLECTION DATA

Plant CCSD 272
Location Unit 2 stack
Date 4/11/90
Run Number 4
Operator DK/ml
Sample Box ID See box
Meter Box ID 004
Probe ID 4
Filter # 3.5

Meter ID 1.014
Meter ΔH 1.87
Pilot C.F. 0.84
Assumed Moisture % 5
Nozzle Diameter in. 0.228
C Factor 5
Ambient Temperature 5
Barometric Pressure 5
Silica Gel # 5

Static Pressure:
Traverse Pt. B-5 B-8
Pwake -0.23
Pstatic -0.28
Water Collected:
Impingers, ml.
Silica Gel, gms.

Traverse Point Number	Sampling Time min.	Stack Temp. (T _s) °F	Stack ΔP in. H ₂ O	Orifice ΔH in. H ₂ O	Meter Reading (V _m) ft ³	Dry Gas Meter Temp.		Sample Box Temp. °F	Probe Temp. °F	Impinger Outlet °F	Pump Vac. in Hg.
						T in °F	T out °F				
B1	5	120	0.25	1.25	6.6	85	80	-	218	68	27
2	10	136	0.35	1.70	10.0	90	82	-	217	68	3
3	15	136	0.37	1.80	13.5	93	82	-	259	70	5
4	20	133	0.37	1.80	17.3	98	83	-	219	73	5
5	25	129	0.38	1.85		101	84	-	207	73	5.5
6	30	136	0.43	2.6	24.8	102	85	-	217	74	6
7	35	156	0.47	2.30	28.8	105	86	-	235	73	7
8	40	167	0.48	2.35	33.0	108	87	-	216	72	7
9	45	173	0.51	2.50	37.1	109	89	-	233	73	7.5
10	50	173	0.55	2.75	41.5	108	90	-	231	73	8
11	55	175	0.58	2.85	45.8	110	90	-	233	74	8.5
12	60	178	0.58	2.85	105.0	109	91	-	240	74	8.5
13											
Averages		157.17	0.69	2.36	96.63	90.81		N/A	229.54	69.5	6.73

FLUE GAS ANALYSES FIELD DATA

Plant ID: CCCSA

Date: 4/11/59

Quality Control

Leak check - all components must pass

O₂/QC gas analysis results

Pre-test		Post-test
☒	CO ₂ Pipette	☒
☒	O ₂ pipette	☒
☒	CO pipette	☒
☒	Sample burette	☒

Gas ID	Run #	CO ₂	CO ₂ +O ₂	O ₂	CO
Ambient	2	0.0	20.8	20.8	
	3				

ORSAT ANALYSES DATA

Sample Bag ID	CO ₂ %	CO ₂ + O ₂	O ₂ %	CO ₂ + O ₂ + CO	CO %	Fo
#08						
(Test 4)	a) 5.7	19.9	14.2			
	b) 5.4	19.7	14.3			
	c) 5.8	20.1	14.3			
	d) 5.6	19.8	14.2			
	Avg 5.7		14.3			
#06						
(Test 5)	5.9	20.2	14.3			
	6.0	20.3	14.3			
	5.8	19.8	14.0			
	5.8	19.8	14.0			
	Avg 5.8		14.0			

FLUE GAS ANALYSES FIELD DATA

Plant ID: CCSD

Date: 4/12/90

Quality Control:

Leak check - all components must pass

O₂/QC gas analysis results.

Pre-test		Post-test	Gas ID	Run #	CO ₂	CO ₂ +O ₂	O ₂	CO
☒	CO ₂ Pipette	_____		1				
☒	O ₂ pipette	_____		2				
_____	CO pipette	_____		3				
_____	Sample burette	_____						

ORSAT ANALYSES DATA

Sample Bag ID	CO ₂ %	CO ₂ + H ₂	O ₂ %	CO ₂ + O ₂ + CO	CO %	Fe
Test 6						
MMT						
GT5#102	5.4	19.9	14.5			
HR	5.3	20.0	14.7			
AR	5.4	20.1	14.7			
Avg	5.4		14.6			
Test 6						
GT5#102	5.2	20.0	14.8			
MMT	5.2	20.4	14.7			
AR	5.2	20.0	14.9			
Avg	5.2		14.8			
Test 7						
-#09	5.0	20.0	15.2			
	5.1	20.3	15.2			
	5.0	20.2	15.2			
Avg	5.0		15.2			
#101						
(TEST 8)	5.3	20.1	14.8			
	5.4	20.0	14.6			
	5.5	20.3	14.8			
Avg	5.4		14.7			



Galson Laboratories

LABORATORY ANALYSIS REPORT

6601 Kirkville Road
E. Syracuse, NY 13057
Tel: (315) 432-0506
1-800-950-0506

Client: COCSD
Task Number: 90041304
Location: MARTINEZ, CA

Job Number: SE034LL
Date Sampled: 11-APR-1990

HEXAVALENT CHROMIUM STACK

Sample ID	Lab ID	TOTAL UG
TEST #4	J8601	<7
TEST #5	J8602	<8
TEST #6	J8603	<8
BLANK	J8604BL	<7

J8601 SPIKE 38% RECOVERY

(<) - Less Than
(>) - Greater Than
NA - Not Applicable
ND - Not detectable
NS - Not specified
MG - Milligrams
L - Liters
M³ - Cubic Meter
MG/M³ - Milligrams Per Cubic Meter
PPM - Parts Per Million
UG - Micrograms
NG - Nanograms
BL - Blank

Method(s): CARB 425
Footnotes:

Submitted by: DD
Approved by: J. Brakena
Date Analyzed: 13-APR-1990

PCDD/PCDF and PAH Emission Data

3.0 Analytical Results

The results generated for each of the sample trains submitted under this project are presented ahead.

Prior to analysis all glassware was thoroughly washed with soap followed by solvent rinses. The glassware was water rinsed again then soaked in chromic acid for one hour. This was followed by additional water rinses and the glassware then dried overnight at 300 °C. In addition all vials and rotary evaporation glassware were similarly cleaned. Unfortunately appreciable levels of naphthalene were still evident in our method blank. Subsequent to these analyses all glassware have been treated with nitric acid which has basically eliminated the problem. The travel blank itself gave the highest level of naphthalene at 810 ug. This in itself may be directly related to the particular XAD resin but cannot be ascertained with any certainty. The surrogate recovery for $^{13}\text{C}_{12}$ benzo(a)pyrene could not be determined due to a large co-eluting peak. No positives were noted for any PCDD/PCDF at the detection levels indicated in the data table. Test #7 and #9 had relatively lower recoveries of the field surrogate $^{37}\text{Cl}_4$ -2,3,7,8-TCDF, 30 and 37% respectively, but in both cases the other field spike, $^{13}\text{C}_{12}$ -1,2,3,4,6,7,8-H7CDF recovered well (89 and 110%).

ANALYTICAL RESULTS REPORT

CLIENT INFORMATION

Name: GALSON TECHNICAL SERVICES
LAB INFORMATION

Contact: OC

Project: AN898849

Date: May.24 1990

Notes: "-" = Not Analyzed
"<" = Less than MDL

Component	MDL	Units	TEST#7	TEST#8	TEST#9	TEST#10	BLANK
			Client ID: 04/17/90 Lab ID: 008519 90	4/17/90 008520 90	4/17/90 008521 90	04/17/90 008522 90	04/17/90 008523 90
2,3,7,8-Tetrachlorodibenzofuran		ng	<0.026	<0.040	<0.038	<0.12	<0.10
2,3,7,8-Tetrachlorodibenzo-p-dioxin			<0.034	<0.090	<0.084	<0.15	<0.22
1,2,3,7,8-Pentachlorodibenzofuran			<0.068	<0.060	<0.080	<0.084	<0.090
2,3,4,7,8-Pentachlorodibenzofuran			<0.070	<0.061	<0.079	<0.090	<0.088
1,2,3,7,8-Pentachlorodibenzo-p-dioxin			<0.094	<0.079	<0.072	<0.088	<0.10
1,2,3,4,7,8-Hexachlorodibenzofuran			<0.042	<0.044	<0.038	<0.056	<0.058
1,2,3,6,7,8-Hexachlorodibenzofuran			<0.042	<0.045	<0.040	<0.056	<0.059
2,3,4,6,7,8-Hexachlorodibenzofuran			<0.041	<0.045	<0.040	<0.054	<0.059
1,2,3,7,8,9-Hexachlorodibenzofuran			<0.042	<0.044	<0.039	<0.054	<0.058
1,2,3,4,7,8-Hexachlorodibenzo-p-dioxin			<0.079	<0.065	<0.090	<0.080	<0.081
1,2,3,6,7,8-Hexachlorodibenzo-p-dioxin			<0.079	<0.067	<0.092	<0.080	<0.085
1,2,3,7,8,9-Hexachlorodibenzo-p-dioxin			<0.079	<0.065	<0.092	<0.082	<0.084
1,2,3,4,6,7,8-Heptachlorodibenzofuran			<0.055	<0.072	<0.055	<0.16	<0.11
1,2,3,4,7,8,9-Heptachlorodibenzofuran			<0.056	<0.075	<0.054	<0.17	<0.11
1,2,3,4,6,7,8-Heptachlorodibenzo-p-dioxin			<0.085	<0.18	<0.082	<0.13	<0.20
1,2,3,4,6,7,8,9-Octachlorodibenzofuran			<0.099	<0.11	<0.10	<0.13	<0.13
1,2,3,4,6,7,8,9-Octachlorodibenzo-p-dioxin			<0.17	<0.15	<0.13	<0.18	<0.18
Total C14 Dibenzo-p-dioxins		ng	<0.034	<0.092	<0.11	<0.17	<0.23
Total C15 Dibenzo-p-dioxins			<0.094	<0.08	<0.073	<0.15	<0.1
Total C16 Dibenzo-p-dioxins			<0.079	<0.067	<0.092	<0.083	<0.084
Total C17 Dibenzo-p-dioxins			<0.085	<0.18	<0.082	<0.14	<0.2
C18 Dibenzo-p-dioxin			<0.17	<0.15	<0.13	<0.18	<0.18
Total C14 Dibenzofurans			<0.026	<0.042	<0.038	<0.16	0.1
Total C15 Dibenzofurans			<0.071	<0.061	<0.14	<0.094	<0.095
Total C16 Dibenzofurans			<0.042	<0.045	<0.041	<0.056	<0.059
Total C17 Dibenzofurans			<0.056	<0.075	<0.055	<0.17	<0.11
C18 Dibenzofuran			<0.099	<0.11	<0.10	<0.13	<0.13
Surrogate Recoveries %							
2,3,7,8-T4CDD 13C-12			86	75	110	140	140
2,3,7,8-T4CDD 37Cl-4			30	110	37	93	89
2,3,7,8-T4CDF 13C-12			120	75	110	81	99
1,2,3,7,8-P5CDD 13C-12			94	41	110	110	110
1,2,3,6,7,8-H6CDD 13C-12			100	100	100	100	100
1,2,3,4,6,7,8-H7CF 13C-12			89	87	110	64	70
1,2,3,4,6,7,8-H7CDD 13C12			90	110	110	92	86
OCDD 13C12			98	92	110	92	91

4.0 Quality Control /Quality Assurance (QA/QC)

A complete QA/QC program is employed by ZENON. The elements of this program and a brief discussion of each of the elements are presented below:

Sample Custody

Strict chain of custody is maintained for samples analysed in this project. Samples received from the field were signed off upon delivery and immediately entered into ZENON's lab information system. Prior to extraction, samples were stored under refrigeration in a secure area. All technologists working on this project have kept accurate records of all actions taken with the samples. ZENON also has a security system in place that ensures unauthorized entry into the lab area is immediately known and appropriate staff and police are contacted.

Method blanks

A method blank is an analysis incorporating all aspects of the analysis, excluding the sample. Its value is to identify the presence of glassware, reagent or instrumentation induced contamination. In this study, a method blank was processed for the group samples. The data generated are not corrected for lab blank.

Standards -Internal, Surrogate & External

ZENON uses both native and labelled PCDD/DF and PAH standards as identified in the CARB protocols. Every sample was fortified with surrogate standards from each contaminant group prior to the start of analysis and each extract was fortified with an internal standard just prior to injection. Three point calibrations were used to define the response curve characteristics.

Surrogate recoveries were generally acceptable, with the exception of

$^{13}\text{C}_{12}$. No recoveries were available due to the presence of a large co-eluting peak which was not removed by the alumina clean-up. Two samples gave marginally lower recoveries on one of the two dioxin surrogates (Test #7 and #9) yet in both cases the other surrogate gave good recoveries (89 and 110%).

SUMMARY OF TEST DATA - PCDD/PCDF AND PAH EMISSIONS

PLANT: CCCSD

STACK #: INCINERATOR #2 EXHAUST

	<u>RUN #7</u>	<u>RUN #8</u>	<u>RUN #9</u>	<u>RUN #10</u>
NUMBER OF SAMPLING POINTS	24	24	24	24
DURATION OF THE RUN, MINUTES	192	192	192	192
SAMPLING NOZZLE DIAMETER, INCHES	0.23	0.23	0.23	0.23
PITOT CALIBRATION FACTOR (CF)	0.84	0.84	0.84	0.84
METER CALIBRATION FACTOR, GAMMA	1.006	1.006	1.006	1.006
STACK DIAMETER, INCHES	41	41	41	41
AMBIENT AIR TEMPERATURE, °F	70	70	70	70
BAROMETRIC PRESSURE, INCHES HG	30.11	30.11	30.02	30.02
AVG STATIC PRES IN FLUE, INCHES H ₂ O	-0.18	-0.14	-0.09	-0.13
ABSOLUTE PRES IN FLUE (P(S)), INCHES HG	30.10	30.10	30.01	30.01
AVG STACK VELOCITY HEAD, SQRT(ΔP)	0.690	0.691	0.688	0.700
AVERAGE ORIFICE (ΔH), INCHES H ₂ O	1.21	1.21	1.19	1.26
VOL SAMPLED (V(M)), FT ³ (METER COND)	118.63	119.67	120.12	118.82
AVERAGE STACK TEMPERATURE (T(S)), °F	148	147	153	152
AVERAGE XAD-2 TEMPERATURE, °F				
AVERAGE IMPINGER OUTLET TEMP, °F	77	67	76	75
AVERAGE METER TEMPERATURE, °F	99	99	107	106
AVERAGE METER VACUUM, INCHES HG	6.9	9.5	9.9	6.7
VOLUME OF WATER CONDENSED (V(LC)), ML	20.2	57.4	46.5	68.1
SPECIFIC GRAVITY OF FLUE GAS (SG)	1.013	1.008	1.010	1.004
ORSAT ANALYSIS:				
• % CO ₂	5.0	5.4	5.4	4.9
• % O ₂	15.2	14.7	14.8	15.1
• % CO	0.0	0.0	0.0	0.0

SAMPLING DATA & CALCULATIONS - PCDD/PCDF AND PAH EMISSIONS

PLANT: CCCSD		STACK #: INCINERATOR #2 EXHAUST			
		RUN #7	RUN #8	RUN #9	RUN #10
A. AREA OF STACK, FT ²		9.17	9.17	9.17	9.17
B. VOLUME SAMPLED (METER COND.), FT ³		118.63	119.67	120.12	118.82
C. VOLUME SAMPLED (STANDARD COND.), SCF	$\frac{B \cdot \text{GAMMA} \cdot [P(\text{BAR}) + (\Delta H / 13.6)] \cdot 530}{(29.92) \cdot [T(M)]}$	114.28	115.30	113.62	112.66
D. VOLUME OF LIQUID WATER CONDENSED, ML		20.2	57.4	46.5	68.1
E. VAPOR VOLUME OF WATER CONDENSED, SCF (STD. CONDITIONS), D=0.04728		0.96	2.71	2.20	3.22
F. MOISTURE, % (E/(E+C)) * 100		0.83	2.30	1.90	2.78
G. AVERAGE VELOCITY IN THE STACK, FPM $4005 \cdot (\text{SQRT}(\text{DP}) \cdot \text{CF} \cdot \text{SQRT}((\text{TS} \cdot 29.92 \cdot 1.0) / (530 \cdot P(S) \cdot \text{SG})))$		2,464	2,471	2,474	2,521
H. STACK GAS FLOW RATE (STACK COND.), CFM (A * G)		22,594	22,652	22,680	23,113
I. STACK GAS FLOW RATE (STD. COND., DRY), DSCFM $H \cdot (1 - (F / 100)) \cdot (530 / T(S)) \cdot (P(S) / 29.92)$		19,635	19,433	19,287	19,527
J. SLUDGE FEED RATE, TONS (DRY)/HOUR		1.5	1.5	1.5	1.5

SAMPLING DATA & CALCULATIONS - PCDD/PCDF AND PAH EMISSIONS

PLANT: CCCSD

STACK #: INCINERATOR #2 EXHAUST

	Run #7	Run #8	Run #9	Run #10
K. PCDD/PCDF Collected, ng.				
2378 TCDD	<0.034	<0.090	<0.084	<0.15
Total TCDD	<0.034	<0.092	<0.11	<0.17
12378 PeCDD	<0.094	<0.079	<0.072	<0.088
Total PeCDD	<0.094	<0.080	<0.073	<0.150
123478 HxCDD	<0.079	<0.065	<0.090	<0.080
123678 HxCDD	<0.079	<0.067	<0.092	<0.080
123789 HxCDD	<0.079	<0.065	<0.092	<0.082
Total HxCDD	<0.079	<0.067	<0.092	<0.083
1234678 HpCDD	<0.085	<0.18	<0.082	<0.13
Total HpCDD	<0.085	<0.18	<0.082	<0.14
Total OCDD	<0.17	<0.15	<0.13	<0.18
Total PCDD	<0.46	<0.57	<0.49	<0.72
2378 TCDF	<0.026	<0.040	<0.038	<0.12
Total TCDF	<0.026	<0.042	<0.038	<0.16
12378 PeCDF	<0.068	<0.060	<0.080	<0.084
23478 PeCDF	<0.070	<0.061	<0.079	<0.090
Total PeCDF	<0.071	<0.061	<0.14	<0.094
123478 HxCDF	<0.042	<0.044	<0.038	<0.056
123678 HxCDF	<0.042	<0.045	<0.040	<0.056
234678 HxCDF	<0.041	<0.045	<0.040	<0.054
123789 HxCDF	<0.042	<0.044	<0.039	<0.054
Total HxCDF	<0.042	<0.045	<0.041	<0.056
1234678 HpCDF	<0.055	<0.072	<0.055	<0.16
1234789 HpCDF	<0.056	<0.075	<0.054	<0.17
Total HpCDF	<0.056	<0.075	<0.055	<0.17
Total OCDF	<0.099	<0.11	<0.10	<0.13
Total PCDF	<0.29	<0.33	<0.37	<0.61

SAMPLING DATA & CALCULATIONS - PCDD/PCDF AND PAH EMISSIONS

PLANT: CCCSD

STACK #: INCINERATOR #2 EXHAUST

	<u>Run #7</u>	<u>Run #8</u>	<u>Run #9</u>	<u>Run #10</u>
L. PCDD/PCDF Concentration, ng/dscm (K*35.3)/C				
2378 TCDD	<0.011	<0.028	<0.026	<0.047
Total TCDD	<0.011	<0.028	<0.034	<0.054
12378 PeCDD	<0.029	<0.024	<0.022	<0.028
Total PeCDD	<0.029	<0.024	<0.023	<0.047
123478 HxCDD	<0.024	<0.020	<0.028	<0.025
123678 HxCDD	<0.024	<0.021	<0.029	<0.025
123789 HxCDD	<0.024	<0.020	<0.029	<0.026
Total HxCDD	<0.024	<0.021	<0.029	<0.026
1234678 HpCDD	<0.026	<0.055	<0.025	<0.041
Total HpCDD	<0.026	<0.055	<0.025	<0.044
Total OCDD	<0.053	<0.046	<0.040	<0.056
Total PCDD	<0.143	<0.175	<0.151	<0.225
2378 TCDF	<0.008	<0.012	<0.012	<0.038
Total TCDF	<0.008	<0.013	<0.012	<0.049
12378 PeCDF	<0.021	<0.018	<0.025	<0.026
23478 PeCDF	<0.022	<0.019	<0.025	<0.028
Total PeCDF	<0.022	<0.019	<0.043	<0.029
123478 HxCDF	<0.013	<0.013	<0.012	<0.018
123678 HxCDF	<0.013	<0.014	<0.012	<0.018
234678 HxCDF	<0.013	<0.014	<0.012	<0.017
123789 HxCDF	<0.013	<0.013	<0.012	<0.017
Total HxCDF	<0.013	<0.014	<0.013	<0.018
1234678 HpCDF	<0.017	<0.022	<0.017	<0.050
1234789 HpCDF	<0.017	<0.023	<0.017	<0.053
Total HpCDF	<0.017	<0.023	<0.017	<0.053
Total OCDF	<0.031	<0.032	<0.031	<0.041
Total PCDF	<0.091	<0.101	<0.116	<0.191

SAMPLING DATA & CALCULATIONS - PCDD/PCDF AND PAH EMISSIONS

PLANT: CCCSD

STACK #: INCINERATOR #2 EXHAUST

	Run #7	Run #8	Run #9	Run #10
M. PCDD/PCDF Emission Rate, $\mu\text{g/hr}$ ($L^3 \cdot I^3 \cdot 60$) / ($35.3 \cdot 1000$)				
2378 TCDD	<0.4	<0.9	<0.9	< 1.6
Total TCDD	<0.4	<0.9	<1.1	<1.8
12378 PeCDD	<1.0	<0.8	<0.7	<0.9
Total PeCDD	<1.0	<0.8	<0.7	<1.6
123478 HxCDD	<0.8	<0.7	<0.9	<0.8
123678 HxCDD	<0.8	<0.7	<0.9	<0.8
123789 HxCDD	<0.8	<0.7	<0.9	<0.9
Total HxCDD	<0.8	<0.7	<0.9	<0.9
1234678 HpCDD	<0.9	<1.8	<0.8	<1.4
Total HpCDD	<0.9	<1.8	<0.8	<1.5
Total OCDD	<1.8	<1.5	<1.3	<1.9
Total PCDD	<4.8	<5.8	<4.9	<7.5
2378 TCDF	<0.3	<0.4	<0.4	<1.2
Total TCDF	<0.3	<0.4	<0.4	<1.6
12378 PeCDF	<0.7	<0.6	<0.8	<0.9
23478 PeCDF	<0.7	<0.6	<0.8	<0.9
Total PeCDF	<0.7	<0.6	<1.4	<1.0
123478 HxCDF	<0.4	<0.4	<0.4	<0.6
123678 HxCDF	<0.4	<0.5	<0.4	<0.6
234678 HxCDF	<0.4	<0.5	<0.4	<0.6
123789 HxCDF	<0.4	<0.4	<0.4	<0.6
Total HxCDF	<0.4	<0.5	<0.4	<0.6
1234678 HpCDF	<0.6	<0.7	<0.6	<1.7
1234789 HpCDF	<0.6	<0.8	<0.5	<1.7
Total HpCDF	<0.6	<0.8	<0.6	<1.7
Total OCDF	<1.0	<1.1	<1.0	<1.4
Total PCDF	<3.0	<3.3	<3.8	<6.3

SAMPLING DATA & CALCULATIONS - PCDD/PCDF AND PAH EMISSIONS

PLANT: CCCSD

STACK #: INCINERATOR #2 EXHAUST

	Run #7	Run #8	Run #9	Run #10
N. PCDD/PCDF Emission Rate, µg/ton M / J				
2378 TCDD	<0.2	<0.6	<0.6	<1.0
Total TCDD	<0.2	<0.6	<0.7	<1.2
12378 PeCDD	<0.6	<0.5	<0.5	<0.6
Total PeCDD	<0.6	<0.5	<0.5	<1.0
123478 HxCDD	<0.5	<0.4	<0.6	<0.6
123678 HxCDD	<0.5	<0.5	<0.6	<0.6
123789 HxCDD	<0.5	<0.4	<0.6	<0.6
Total HxCDD	<0.5	<0.5	<0.6	<0.6
1234678 HpCDD	<0.6	<1.2	<0.6	<0.9
Total HpCDD	<0.6	<1.2	<0.6	<1.0
Total OCDD	<1.2	<1.0	<0.9	<1.2
Total PCDD	<3.2	<3.8	<3.3	<5.0
2378 TCDF	<0.2	<0.3	<0.3	<0.8
Total TCDF	<0.2	<0.3	<0.3	<1.1
12378 PeCDF	<0.5	<0.4	<0.5	<0.6
23478 PeCDF	<0.5	<0.4	<0.5	<0.6
Total PeCDF	<0.5	<0.4	<0.9	<0.7
123478 HxCDF	<0.3	<0.3	<0.3	<0.4
123678 HxCDF	<0.3	<0.3	<0.3	<0.4
234678 HxCDF	<0.3	<0.3	<0.3	<0.4
123789 HxCDF	<0.3	<0.3	<0.3	<0.4
Total HxCDF	<0.3	<0.3	<0.3	<0.4
1234678 HpCDF	<0.4	<0.5	<0.4	<1.1
1234789 HpCDF	<0.4	<0.5	<0.4	<1.2
Total HpCDF	<0.4	<0.5	<0.4	<1.2
Total OCDF	<0.7	<0.7	<0.7	<0.9
Total PCDF	<2.0	<2.2	<2.5	<4.2

SAMPLING DATA & CALCULATIONS - PAH EMISSIONS

PLANT: CCCSD

STACK #: INCINERATOR #2 EXHAUST

	RUN #7	RUN #8	RUN #9	RUN #10
O. PAH Quantities ¹ , µg				
Naphthalene	45	45	100	26
Acenaphthylene	< 0.06	< 0.06	< 0.06	< 0.06
Acenaphthene	< 0.06	< 0.06	< 0.06	< 0.06
Fluorene	< 0.06	< 0.06	< 0.06	< 0.06
Phenanthrene	< 0.04	< 0.04	< 0.04	< 0.04
Anthracene	< 0.04	< 0.04	< 0.04	< 0.04
Fluoranthene	< 0.04	< 0.04	< 0.04	< 0.04
Pyrene	< 0.04	< 0.04	< 0.04	< 0.04
Chrysene	< 0.04	< 0.04	< 0.04	< 0.04
Benzo(a)anthracene	< 0.04	< 0.04	< 0.04	< 0.04
Benzo(b)fluoranthene	< 0.04	< 0.04	< 0.04	< 0.04
Benzo(k)fluoranthene	< 0.04	< 0.04	< 0.04	< 0.04
Benzo(a)pyrene	< 0.04	< 0.04	< 0.04	< 0.04
Indeno(1,2,3-cd)pyrene	< 0.04	< 0.04	< 0.04	< 0.04
Dibenzo(a,h)anthracene	< 0.06	< 0.06	< 0.06	< 0.06
Benzo(g,h,i)perylene	< 0.04	< 0.04	< 0.04	< 0.04

P. PAH Concentration, µg/dscm
 (O * 35.3) / C

Naphthalene	14	14	31	8
Acenaphthylene	< 0.02	< 0.02	< 0.02	< 0.02
Acenaphthene	< 0.02	< 0.02	< 0.02	< 0.02
Fluorene	< 0.02	< 0.02	< 0.02	< 0.02
Phenanthrene	< 0.01	< 0.01	< 0.01	< 0.01
Anthracene	< 0.01	< 0.01	< 0.01	< 0.01
Fluoranthene	< 0.01	< 0.01	< 0.01	< 0.01
Pyrene	< 0.01	< 0.01	< 0.01	< 0.01
Chrysene	< 0.01	< 0.01	< 0.01	< 0.01
Benzo(a)anthracene	< 0.01	< 0.01	< 0.01	< 0.01
Benzo(b)fluoranthene	< 0.01	< 0.01	< 0.01	< 0.01
Benzo(k)fluoranthene	< 0.01	< 0.01	< 0.01	< 0.01
Benzo(a)pyrene	< 0.01	< 0.01	< 0.01	< 0.01
Indeno(1,2,3-cd)pyrene	< 0.01	< 0.01	< 0.01	< 0.01
Dibenzo(a,h)anthracene	< 0.02	< 0.02	< 0.02	< 0.02
Benzo(g,h,i)perylene	< 0.01	< 0.01	< 0.01	< 0.01

¹ PAH quantities are not corrected for blank quantities. Naphthalene was the only compound determined to be present in the blank; refer to the laboratory data presented in Appendix VI for additional detail.

SAMPLING DATA & CALCULATIONS - PCDD/PCDF AND PAH EMISSIONS

PLANT: CCCSD

STACK #: INCINERATOR #2 EXHAUST

	<u>RUN #7</u>	<u>RUN #8</u>	<u>RUN #9</u>	<u>RUN #10</u>
Q. PAH Emission Rate, mg/hr (P*I*60)/(35.3*1000)				
Naphthalene	464	455	1020	270
Acenaphthylene	< 0.6	< 0.6	< 0.6	< 0.6
Acenaphthene	< 0.6	< 0.6	< 0.6	< 0.6
Fluorene	< 0.6	< 0.6	< 0.6	< 0.6
Phenanthrene	< 0.4	< 0.4	< 0.4	< 0.4
Anthracene	< 0.4	< 0.4	< 0.4	< 0.4
Fluoranthene	< 0.4	< 0.4	< 0.4	< 0.4
Pyrene	< 0.4	< 0.4	< 0.4	< 0.4
Chrysene	< 0.4	< 0.4	< 0.4	< 0.4
Benzo(a)anthracene	< 0.4	< 0.4	< 0.4	< 0.4
Benzo(b)fluoranthene	< 0.4	< 0.4	< 0.4	< 0.4
Benzo(k)fluoranthene	< 0.4	< 0.4	< 0.4	< 0.4
Benzo(a)pyrene	< 0.4	< 0.4	< 0.4	< 0.4
Indeno(1,2,3-cd)pyrene	< 0.4	< 0.4	< 0.4	< 0.4
Dibenzo(a,h)anthracene	< 0.6	< 0.6	< 0.6	< 0.6
Benzo(g,h,i)perylene	< 0.4	< 0.4	< 0.4	< 0.4

R. PAH Emission Ratio, mg/ton, dry
Q / J

Naphthalene	309	303	679	18
Acenaphthylene	< 0.4	< 0.4	< 0.4	< 0.4
Acenaphthene	< 0.4	< 0.4	< 0.4	< 0.4
Fluorene	< 0.4	< 0.4	< 0.4	< 0.4
Phenanthrene	< 0.3	< 0.3	< 0.3	< 0.3
Anthracene	< 0.3	< 0.3	< 0.3	< 0.3
Fluoranthene	< 0.3	< 0.3	< 0.3	< 0.3
Pyrene	< 0.3	< 0.3	< 0.3	< 0.3
Chrysene	< 0.3	< 0.3	< 0.3	< 0.3
Benzo(a)anthracene	< 0.3	< 0.3	< 0.3	< 0.3
Benzo(b)fluoranthene	< 0.3	< 0.3	< 0.3	< 0.3
Benzo(k)fluoranthene	< 0.3	< 0.3	< 0.3	< 0.3
Benzo(a)pyrene	< 0.3	< 0.3	< 0.3	< 0.3
Indeno(1,2,3-cd)pyrene	< 0.3	< 0.3	< 0.3	< 0.3
Dibenzo(a,h)anthracene	< 0.4	< 0.4	< 0.4	< 0.4
Benzo(g,h,i)perylene	< 0.3	< 0.3	< 0.3	< 0.3

ISOKINETIC VARIATION CALCULATION

PLANT: CCCSD

STACK #: INCINERATOR #2 EXHAUST

PARAMETER	RUN #7	RUN #8	RUN #9	RUN #10
T(S), °R	608	607	613	612
V(LC), ML	20.2	57.4	46.5	68.1
GAMMA	1.006	1.006	1.006	1.006
V(M), FT ³	118.63	119.67	120.12	118.82
T(M), °R	559	559	567	566
P(BAR)+(ΔH/13.6), IN. HG	30.2	30.2	30.11	30.11
V(S), FPM	2,464	2,471	2,474	2,521
P(S), IN. HG	30.10	30.10	30.01	30.01
A(N), FT ²	0.0003	0.0003	0.0003	0.0003
THETA, MINUTES	192	192	192	192
I (PERCENT OF ISOKINETIC) ¹	96.3	98.2	97.5	95.5

¹ $I = \frac{(T(S) \cdot 100((0.00267 \cdot V(CL)) + (V(M)/T(M)) \cdot GAMMA \cdot (P(BAR) + (\Delta H/13.6))))}{(THETA \cdot V(S) \cdot P(S) \cdot A(N))}$

ORSAT DATA AND GAS DENSITY CALCULATIONS

PLANT: CCCSD

STACK #: INCINERATOR #2 EXHAUST

PARAMETER	RUN #7		RUN #8		RUN #9		RUN #10	
	DRY BASIS	WET BASIS	DRY BASIS	WET BASIS	DRY BASIS	WET BASIS	DRY BASIS	WET BASIS
CO ₂	5.00	4.96	5.40	5.28	5.40	5.30	4.90	4.76
O ₂	15.20	15.07	14.70	14.36	14.80	14.52	15.10	14.68
CO	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
N ₂	79.80	79.14	79.90	78.06	79.80	78.29	80.00	77.78
H ₂ O	---	0.83	---	2.30	---	1.90	---	2.78
MOLECULAR WEIGHT ¹	---	29.31	---	29.19	---	29.24	---	29.07
SPECIFIC GRAVITY OF GAS ²	---	1.013	---	1.008	---	1.010	---	1.004

¹ Calculated from the equation:

$$\text{Molecular Weight} = 0.44(\% \text{CO}_2) + 0.32(\% \text{O}_2) + 0.28(\% \text{N}_2 + \% \text{CO}) + 0.18(\% \text{H}_2\text{O})$$

² SG= Molecular Weight of Stack Gas/ Molecular Weight of Air (28.95 gm/gm-mole)

 $\frac{3}{4}$

SAMPLE COLLECTION DATA

Plant CCSD
Location Dair #2 Steck
Date 4/12/92
Run Number 107
Operator MA
Sample Box ID _____
Meter Box ID 005
Probe ID _____
Filter # _____

Meter Ø —
Meter Δ H@
Pilot C.F. —
Assumed M
Nozzle Diam
C Factor —
Ambient Te
Barometric
Silica Gel #

● 1997

Static Pressure: $B-S^*$
Traverse Pt. $B-S$
Pwaka -0.26
 $\frac{B-9}{-0.46}$

Water Collected:

Silica Gel, 0.075 mm.

[illegible]



Comments: Test 1 k Rate
Post 8 cfm @
0.008 cfm @
11 in Hg

SAMPLE COLLECTION DATA

Plant CCCSP
Location Unit 2 Stack
Date _____
Run Number _____
Operator _____
Sample Box ID _____
Meter Box ID _____
Probe ID _____
Filter # 720.5

Meter ID _____
Meter Δ H @ _____
Pilot C.F. _____
Assumed Moisture % _____
Nozzle Diameter in. _____
C Factor _____
Ambient Temperature _____
Barometric Pressure _____
Silica Gel # _____

Static Pressure:

Traverse Pt. _____

Pwake _____

Pstatic _____

Water Collected: _____

Impingers, ml. _____

Silica Gel, gms. _____

Orsat 09

Traverse Point Number	Sampling Time min.	Stack Temp. (Ts) °F	Stack Δ P in. H ₂ O	Orifice Δ H in. H ₂ O	Meter Reading (Vm) ft ³	Dry Gas Meter Temp.		Sample Box Temp. °F	Probe Temp. °F	Impinger Outlet °F	Pump Vac. in Hg.
						T in °F	T out °F				
B10	76	177	0.65	1.60	723.4	111	99	246	246	80/52	8
10	80	183	0.55	1.35	726.1	110	99	248	249	80/58	7
11	84	184	0.56	1.40	728.8	112	99	248	252	82/64	8
11	88	175	0.59	1.45	731.6	112	101	252	253	84/71	8
12	92	174	0.59	1.45	734.4	112	101	252	251	-162	7.5
12	96	174	0.60	1.50	737.8	112	101	254	250	77/48	8
Averages		148.10	0.69	1.21	118.63		98.64	243-25	243.79	76.83 / 54.13	6.9



Galson
Technical Services

2/4 SAMPLE COLLECTION DATA

Plant CCSD
 Location 4413
 Date 4/12/83
 Run Number PAH
 Operator DR
 Sample Box ID _____
 Meter Box ID _____
 Probe ID _____
 Filter # 7107

Meter 0
 Meter $\Delta H @$ _____
 Pilot C.F. _____
 Assumed Moisture % _____
 Nozzle Diameter in. _____
 C Factor _____
 Ambient Temperature _____
 Barometric Pressure _____
 Silica Gel # _____

Static Pressure: _____

Traverse Pt. *B8 0.25

Pwake -0.26 _____

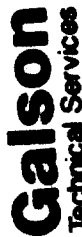
Pstatic _____

Water Collected: _____

Impingers, ml. _____

Silica Gel, gms. _____

[illegible]



三

SAMPLE COLLECTION DATA

0501
3/4

Plant Unit 2 stack
Location 4/12/00
Date 4/12/00
Run Number 062
Operator DR
Sample Box ID 062
Meter Box ID 003
Probe ID _____
Filter # 0032

Meter $\bar{O}$ _____
 Meter $\Delta H @$ _____
 Pilot C.F. _____
 Assumed Moisture % _____
 Nozzle Diameter in. _____
 C Factor _____
 Ambient Temperature _____
 Barometric Pressure _____
 Silica Gel # _____

Static Pressure:

Traverse Pt. A4 #A7
-0.31 -0.32

Plastic.

Water Collected:

Impingers, ml.

Cilica Gel. oms.

[illegible]



Galson
Technical Services

$$4/4$$

Plant CCSD
Location Unit 2 S10A
Date 06/27/03
Run Number 11418
Operator VR
Sample Box ID 03-2
Meter Box ID 003
Probe ID _____
Filter # 337

Meter Ø 1.000
 Meter ΔH@ 1.122
 Pilot C.F. _____
 Assumed Moisture % _____
 Nozzle Diameter in. _____
 C Factor _____
 Ambient Temperature _____
 Barometric Pressure _____
 Silica Gel # _____

Traverse Pt. _____

Pwako _____

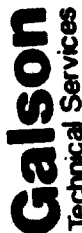
Psaltic —————

Water Collected:

—
inners. ml.

Calva Cal. ans. —

[illegible]



FLYER

594.5

SAMPLE COLLECTION DATA

Plant	CCS02/4	Meter Ø	1.006
Location	Unit 2	Meter ΔH@	1.72
Date	7/13/90	Pilot C.F.	
Run Number	999H	Assumed Moisture %	
Operator	DR	Nozzle Diameter in.	
Sample Box ID		C Factor	
Meter Box ID		Ambient Temperature	
Probe ID		Barometric Pressure	
		Silica Gel #	

Static Pressure:

Traverse Pt. X 110.119

Pwako 0820 070

Plastic —

Water Collected:

Impingers, ml.

Cellulose Gel, gums.

●

[illegible]



Galson

Comments:

SAMPLE COLLECTION DATA

Plant CCCSO
Location MOIST #2/STARK
Date 4/13/90
Run Number 999H
Operator DR
Sample Box ID _____
Meter Box ID _____
Probe ID _____
Filter # ATK 999

640 816

Static Pressure:

Traversa Pl. *B6

Pwako 218

Polibac

Water Collected:

Impingers, ml.

Silica Gel, gms.

[illegible]



Comments: Test
Leak rate
0.006cfm
0.015inHg

4/4 SAMPLE COLLECTION DATA

Plant CCSD
Location UNIT 2 Stack
Date 4/23/94
Run Number DR
Operator PTA
Sample Box ID _____
Meter Box ID _____
Probe ID _____
Filter # 945.2

Meter ID _____
Meter ΔH@ _____
Pilot C.F. _____
Assumed Moisture % _____
Nozzle Diameter in. _____
C Factor _____
Ambient Temperature _____
Barometric Pressure _____
Silica Gel # _____

Static Pressure: _____
Traverse Pt. XB9
Pwake -0.29
Pstatic _____
Water Collected: _____
Impingers, ml. _____
Silica Gel, gms. _____

Imp/NAD

Traverse Point Number	Sampling Time min.	Stack Temp. (Ts) °F	Stack ΔP in. H2O	Orifice ΔH in. H2O	Meter Reading (Vn) ft3	Dry Gas Meter Temp.		Sample Box Temp. °F	Probe Temp. °F	Impinger Outlet °F	Pump Vac. in Hg.
						T in °F	T out °F				
B7	52	162	0.51	1.25	947.8	115	106	256	234	78/58	10.5
7	56	163	0.51	1.25	950.3	116	106	256	235	80/60	10.5
B8	60	170	0.55	1.35	953.0	116	107	257	236	80/60	11
8	64	168	0.55	1.35	955.6	117	107	256	237	79/59	11
*9	68	172	0.59	1.45	958.4	116	107	255	235	78/57	11.5
9	72	172	0.60	1.50	961.2	115	107	256	232	79/58	12
10	76	171	0.61	1.50	964.0	118	107	259	230	79/58	12
10	80	170	0.62	1.55	965	121	107	257	222	80/59	13
11	84	172	0.66	1.65	—	121	108	258	225	80/60	13.5
11	88	172	0.66	1.65	972.8	120	108	258	226	82/63	13.5
11	92	171	0.69	1.70	—	120	109	258	226	84/67	14
12	96	171	0.68	1.70	978.742	121	109	258	225	84/69	14
134012											
Averages		153.31	0.688	1.19	120.12	107.23		253.31	238.02	76.25	9.91



Comments:

02-49
02-15.1

SAMPLE COLLECTION DATA

Plant CCSD
Location 4th St Stack
Date 4/13/90
Run Number 10 PH
Operator 28-2
Sample Box ID 805
Meter Box ID 4
Probe ID 974913
Filter # 974913

Meter 1.006
Meter ΔH 0.84
Pilot C.F. 0.84
Assumed Moisture % 2.30
Nozzle Diameter in. 0.84
C Factor 2.30
Ambient Temperature 70
Barometric Pressure 30.02
Silica Gel # 35.3

Static Pressure: BS
Traverse Pt. BS
Pwake 0.19
Pstatic 35.3
Water Collected: 32.5
Impingers, ml. 68.1
Silica Gel, gms. 35.3

Traverse Point Number	Sampling Time min.	Stack Temp. (Ts) °F	Stack ΔP in. H ₂ O	Orifice ΔH in. H ₂ O	Meter Reading (Nm) ft ³	Dry Gas Meter Temp.		Sample Box Temp. °F	Probe Temp. °F	Impinger Outlets °F	Impinger Pump Vac. in Hg.
						T in °F	T out °F				
B1	4	127	0.25	0.57	981.6	98	104	238	253	80/76	4
B1	8	126	0.25	0.56	983.4	100	104	247	243	80/76	3.5
B2	12	130	0.32	0.80		103	104	247	246	80/76	4.5
B2	16	131	0.31	0.78	977.6	106	104	250	240	80/76	5
B3	20	128	0.36	0.90		108	104	251	235	80/76	5.5
B3	24	128	0.35	0.88	992.0	110	105	253	235	80/76	5.5
B4	28	124	0.35	0.88		111	105	255	232	80/76	5.5
B4	32	128	0.35	0.86	996.3	110	105	255	230	80/76	6
B5	36	127	0.37	0.93		111	105	255	229	80/76	6
B5	40	127	0.36	0.90	1002.9	109	105	251	239	80/76	6
B6	44	133	0.38	0.95	1006.1	109	104	253	241	80/76	6
B6	48	133	0.39	0.98	1008.7	109	104	252	244	80/76	6.3
B7	52	160	0.48	1.20		109	104	252			
B7	56										
Averages											

Note: X10.2 Temperature reading suspect



211

SAMPLE COLLECTION DATA

$$\frac{7}{24}$$

Plant CCCSO
Location Unit 2 Stack
Date 4/13/90
Run Number 10PAH
Operator _____
Sample Box ID _____
Meter Box ID _____
Probe ID _____
Filter # _____

Static Pressure:

Traverse Pt. _____

Pwako _____

Plastic —

Water Collected:

Impingers. ml.

Silica Gel, gms.

● 1997年

[illegible]

4/4

SAMPLE COLLECTION DATA



Comments:

Test back
Date 0.0060
09.11.15

Plant

Location

Date

Run Number

Operator

Sample Box ID

Meter Box ID

Probe ID

Filter #

Meter Ø

Meter ΔH@

Pilot C.F.

Assumed Moisture %

Nozzle Diameter in.

C Factor

Ambient Temperature

Barometric Pressure

Silica Gel #

Static Pressure:

Traverse Pt. A-8Pwake -0.31

Pstatic

Water Collected:

Impingers, ml.

Silica Gel, gms.

Traverse Point Number	Sampling Time min.	Stack Temp. (Ts) °F	Stack ΔP in. H2O	Orifice ΔH in. H2O	Meter Reading (Vm) ft3	Dry Gas Meter Temp.		Sample Box Temp. °F	Probe Temp. °F	Impinger Outlet °F	Pump Vac. in Hg.
						T in °F	T out °F				
A8	60	151	0.61	1.35	1075.4	113	103	248	235	74/72	8
8#	64	153	0.57	1.45		114	103	248	242	72/70	8
7	68	147	0.53	1.35	1080.75	115	104	247	244	74/72	7.5
9	72	143	0.54	1.35	1083.4	115	104	248	232	74/72	7.5
10	76	141	0.51	1.30		114	104	246	224	75/73	7.5
10	80	143	0.53	1.35	1088.5	113	104	243	229	76/74	7.5
11	84	143	0.49	1.20	1091.2	112	103	242	237	76/75	7
11	88	140	0.50	1.25	1083.7	111	102	241	248	78/76	7
12	92	134	0.47	1.15	1096.25	109	102	241	250	78/76	7
12	96	141	0.47	1.15	1098.732	109	101	238	251	78/72	7
12	100	141	0.47	1.15	1098.732	109	101	238	251	78/72	7
Averages		151.77	0.7	1.26	118.82	105.97		249.21	240.08	75.46	6.73

FLUE GAS ANALYSES FIELD DATA

Plant ID: CCSD-Unit 2

Date: 4/13/90

Quality Control:

Vol - HChrome (Test 6) = 8232

Leak check - all components must pass

O₂/QC gas analysis results

Pre-test	Post-test	Gas ID	Run #	CO ₂	CO ₂ +O ₂	O ₂	CO
CO ₂ Pipette			1				
O ₂ pipette			2				
CO pipette			3				
Sample burette							

ORSAT ANALYSES DATA

Sample Bag ID	CO ₂ %	CO ₂ + O ₂	O ₂ %	CO ₂ + O ₂ + CO	CO %	FO
06	5.4					
Test 9	5.3	19.8	14.7			
	5.3	20.1	14.8			
CMT: GTS 06	5.6	20.0	14.8			
Test #9	5.3	20.2	14.9			
	5.4		14.8			
TEST #10						
GTS #08	1.0					
OR: GTS #02	5.0	20.0	15.0			
	4.8	20.0	15.2			
Test 10	5.0	20.2	15.2			
	4.9		15.1			

CO and THC Emission Data

SAMPLING DATA AND CALCULATIONS - CO AND THC EMISSIONS

Plant: CCCSD

Stack: Unit #2 Exhaust

SAMPLING DATA:

	<u>Run #4</u>	<u>Run #5</u>	<u>Run #6</u>
Stack Gas Moist Content ¹ (%H ₂ O), %	2.3	2.2	2.3
Stack Gas Flow Rate ¹ , DSCFM	19,042	19,583	20,083
Sludge Feed Rate, TPH (dry)	1.7	1.6	1.5
CO Concentration, ppm (dry)	28.9	56.5	61.0
THC Concentration ² , ppm (wet)	10.5	9.6	12.2

CALCULATIONS:

A. Stack Gas Flow Rate, DSCFM	19,042	19,583	20,083
B. Concentration, ppm (dry)			
• CO	28.9	56.5	61.0
• THC ³	10.7	9.8	12.5
C. Sludge Feed Rate, tph (dry)	1.7	1.6	1.5
D. Emission Rate, lbs/hr (B * A * MW ⁴ * 60) / (454,000 * 35.3 * 24.13)			
• CO	2.39	4.81	5.32
• THC	0.51	0.48	0.62
E. Emission Ratio, lbs/ton (dry) D/C			
• CO	1.4	3.0	3.5
• THC	0.3	0.3	0.4

- 1 Based on data collected during the concurrent metals and hexavalent chromium testing; average values were used.
- 2 As methane (CH₄)
- 3 Dry Basis = Wet Basis / (1 - (%H₂O/100))
- 4 Molecular weight (CO) = 28 gm/gm-mole;
 Molecular weight (CH₄) = 16 gm/gm-mole

SAMPLING DATA AND CALCULATIONS - CO AND THC EMISSIONS

Plant: CCCSD

Stack: Unit #2 Exhaust

SAMPLING DATA:

	<u>Run #1</u>	<u>Run #2</u>	<u>Run #3</u>
Stack Gas Moist Content ¹ (%H ₂ O), %	2.9	2.5	2.6
Stack Gas Flow Rate ¹ , DSCFM	19,191	19,475	20,038
Sludge Feed Rate, TPH (dry)	1.7	1.6	1.7
CO Concentration, ppm (dry)	34.5	74.0	25.9
THC Concentration ² , ppm (wet)	12.3	8.9	9.6

CALCULATIONS:

A. Stack Gas Flow Rate, DSCFM	19,191	19,475	20,038
B. Concentration, ppm (dry)			
• CO	34.5	74.0	25.9
• THC ³	12.7	9.1	9.9
C. Sludge Feed Rate, tph (dry)	1.7	1.6	1.7
D. Emission Rate, lbs/hr (B*A*MW ⁴ *60)/(454,000*35.3*24.13)			
• CO	2.88	6.26	2.26
• THC	0.61	0.44	0.49
E. Emission Ratio, lbs/ton (dry) D/C			
• CO	1.7	3.9	1.3
• THC	0.4	0.3	0.3

1 Based on data collected during the concurrent HCl testing.

2 As methane (CH₄)

3 Dry Basis = Wet Basis/(1-(%H₂O/100))

4 Molecular weight (CO) = 28 gm/gm-mole;
 Molecular weight (CH₄) = 16 gm/gm-mole

SAMPLING DATA AND CALCULATIONS - CO AND THC EMISSIONS

Plant: CCCSD

Stack: Unit #2 Exhaust

SAMPLING DATA:

	<u>Run #7</u>	<u>Run #8</u>	<u>Run #9</u>	<u>Run #10</u>
Stack Gas Moist Content ¹ (%H ₂ O), %	0.8	2.3	1.9	2.8
Stack Gas Flow Rate ¹ , DSCFM	19,635	19,433	19,287	19,527
Sludge Feed Rate, TPH (dry)	1.5	1.5	1.5	1.5
CO Concentration, ppm (dry)	50.9	70.8	58.6	39.4 ²
THC Concentration ³ , ppm (wet)	13.5	10.4	15.4	16.8

CALCULATIONS:

A. Stack Gas Flow Rate, DSCFM	19,635	19,433	19,287	19,527
B. Concentration, ppm (dry)				
• CO	50.9	70.8	58.6	39.4
• THC ⁴	13.6	10.6	15.7	17.3
C. Sludge Feed Rate, tph (dry)	1.5	1.5	1.5	1.5
D. Emission Rate, lbs/hr				
(B * A * MW ⁵ * 60) / (454,000 * 35.3 * 24.13)				
• CO	4.34	5.98	4.91	3.34
• THC	0.66	0.51	0.75	0.84
E. Emission Ratio, lbs/ton (dry)				
D/C				
• CO	2.9	4.0	3.3	2.2
• THC	0.4	0.3	0.5	0.6

1 Based on data collected during the concurrent PAH tests.

2 As methane (CH₄).

3 Based on the average concentration monitored during the period, 1455-1744; CO levels exceeded 200 ppm throughout the remainder of the test period (1744-1823).

4 Dry Basis = Wet Basis / (1 - (%H₂O/100))

5 Molecular weight (CO) = 28 gm/gm-mole;

Molecular weight (CH₄) = 16 gm/gm-mole