

Laidlaw Gas Recovery Systems
Newby Island Plant #1
Emissions Testing

Test Date: Sept. 22 & Oct. 9, 1992

BEST ENVIRONMENTAL, INC.

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San Leandro, California 94578

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October 9, 1992

Laidlaw Gas Recovery Systems
39899 Balentine Dr. Suite 275
Newark, CA. 94560

Attn: Mr. Matt L. Nourof, Mechanical Engineer

Subject: Newby Island Plant Site #1 I.C. Engine's Emissions Test

Test Dates: September 22 and October 9, 1992

Sampling Location: Muffler outlets of the #1 and 2 I.C. engines operated at Gas Recovery Systems Newby Island Plant #1 site in Milpitas, California.

Sampling Personnel: Jeff Mesloh and Dan Cartner of BEST ENVIRONMENTAL.

Process Description: Gas Recovery Systems operates seven engines at the Newby Island Plant. The two engines tested were Cooper Superior Model 8G825 I.C. engines with a maximum power rating of 500 KW. During the test runs each engine operated at 450 kilowatts and burned landfill gas fuel.

Test Program: Three thirty minute test runs for NOx, CO, CO2, O2, THC, and TNMHC were performed at the engine muffler 1 & 2 outlets. Stack gas temperatures, moisture content and volumetric flowrates were determined at both locations.

Sampling Methods: The following Source Test Methods of the Bay Area Air Quality Management District (BAAQMD) and the California Air Resources Board (CARB) were used:

Method ST-17	Stack Velocity and Volumetric Flow Rate
Method ST-23	Water Vapor Sampling
CARB 1-100	Continuous NOx, O2, CO2, CO, THC

Instrumentation:

TECO Model 10 NOx analyzer
Horiba Model PIR 2000 CO2 analyzer
Infrared Model IR-2200 O2 analyzer
TECO Model 48 CO analyzer
Bendix Model 8401 Hydrocarbon analyzer
Standard pitot tube, inclined manometer, thermocouple
Calibrated Dry Gas Meter
All Glass Impingers
Hewlett Packard Chart Recorders

Calibrated Omega Temperature Meter

Test Results: Table 1 presents the results of the #1 engine emissions tests. Average NOx concentration and emission rates were 184.3 ppm and 1.60 lbs/hr or 1.14 grams/Bhp-hr. CO concentration and emission rates were 1.0 ppm and 0.01 lbs/hr or 0.004 grams/Bhp-hr. No detectable level of TNMHC was measured.

Table 2 presents the results of the #2 engine emissions tests. Average NOx concentration and emission rates were 500 ppm and 4.16 lbs/hr or 2.97 grams/Bhp-hr. CO concentration and emission rate were 1086 ppm and 5.50 lbs/hr or 3.93 grams/Bhp-hr. No detectable level of TNMHC was measured.

Field data sheets, strip chart recordings, calibration gas certifications and volumetric flowrate calculations are appended to this report. If there are any questions, please call Dan Cartner at (415) 784-0706.

Submitted by



Dan Cartner
Source Test Engineer

Laidlaw
Newby Island
Engine #1

TABLE 1
CEMS TEST RESULTS

TEST LOCATION	1 OUTLET	2 OUTLET	3 OUTLET	AVERAGE
TEST TIME	0926-0956	1002-1032	1038-1108	
TEST DATE	09-22-92	09-22-92	09-22-92	
FLOWRATE, SDCFM	1,212	1,212	1,212	1,212
OUTPUT, KW	450	450	450	
O2, %	0.6	0.6	0.6	0.6
CO2, %	17.0	17.0	17.2	17.07
H2O, %	17.4	17.4	17.4	17.40
NOx, ppm	178.0	187.0	188.0	184.3
NOx, ppm corr. 3%, O2	157.0	164.9	165.8	162.54
NOx, lbs/hr	1.55	1.63	1.64	1.60
NOx, gr/Bhp-hr	1.106	1.162	1.168	1.145
CO, ppm	1.0	1.0	1.0	1.0
CO, lbs/hr	0.01	0.01	0.01	0.01
CO, gr/Bhp-hr	0.004	0.004	0.004	0.004
THC, ppm	1947.0	1688.0	1657.0	1764.00
TNMHC, ppm	< 25.0	< 25.0	< 25.0	< 25.0
TNMHC, lbs/hr	< 0.08	< 0.08	< 0.08	< 0.08
TNMHC, gr/Bhp-hr	< 0.054	< 0.054	< 0.054	< 0.054

WHERE,

NOx = Oxides of Nitrogen
THC = Tot. Hydrocarbons @CH4
TNMHC = Tot. Non-methane Hydrocarbons @CH4
ppm = Parts Per Million Concentration
lbs/hr = Pounds Per Hour Emission Rate
CO = Carbon Monoxide
CO2 = Carbon Monoxide

Calculations,

lbs/hr = ppm x SDCFM x (1.56e-7) x Mol. Wt.
gr/Bhp-hr = (lbs/hr) (453.6g/lb) / (kw/(.746 x 95%))

LAIDLAW
Newby Island
Engine #2

TABLE 2
CEMS TEST RESULTS

TEST TEST LOCATION	1 OUTLET	2 OUTLET	3 OUTLET	AVERAGE
TEST TIME	1142-1213	1220-1250	1254-1324	
TEST DATE	10-09-92	10-09-92	10-09-92	
FLOWRATE, SDCFM	1,160	1,160	1,160	1,160
OUTPUT, KW	450	450	450	
O2, %	1.5	1.4	1.5	1.5
CO2, %	17.2	17.4	17.4	17.33
H2O, %	16.6	16.6	16.6	16.60
NOx, ppm	520.0	480.0	500.0	500.0
NOx, ppm corr. 3%, O2	479.8	440.6	461.3	460.58
NOx, lbs/hr	4.33	4.00	4.16	4.16
NOx, gr/Bhp-hr	3.092	2.854	2.973	2.973
CO, ppm	1138.0	1045.0	1075.0	1086.0
CO, lbs/hr	5.77	5.29	5.45	5.50
CO, gr/Bhp-hr	4.119	3.783	3.891	3.931
THC, ppm	25.0	25.0	25.0	25.00
TNMHC, ppm	< 5.0	< 5.0	< 5.0	< 5.0
TNMHC, lbs/hr	< 0.01	< 0.01	< 0.01	< 0.01
TNMHC, gr/Bhp-hr	< 0.010	< 0.010	< 0.010	< 0.010

WHERE,

NOx = Oxides of Nitrogen
THC = Tot. Hydrocarbons @CH4
TNMHC = Tot. Non-methane Hydrocarbons @CH4
ppm = Parts Per Million Concentration
lbs/hr = Pounds Per Hour Emission Rate
CO = Carbon Monoxide
CO2 = Carbon Monoxide

Calculations,

lbs/hr = ppm x SDCFM x (1.56e-7) x Mol. Wt.
gr/Bhp-hr = (lbs/hr) (453.6g/lb) / (kw/(.746 x 95%))

APPENDIX

BEST ENVIRONMENTAL
STACK VOLUMETRIC FLOW RATE DETERMINATION

LAIDLAW
Engine #1

Date: 9-22-92
Location: Outlet
Time: 1010

1. Temperature of Stack (Ts)	1294 F
2. Square Root of Delta P ($\sqrt{P}$)	1.109 "H2O
3. Barometric Pressure (Pb)	29.98 "Hg
4. Stack Static Pressure	4 "H2O
5. Percent of H2O in Stack	17.5 %
6. Mol. Weight of Stack Gas (Mws)	28.51
A. Percent O2	0.6 %
B. Percent CO2	17 %
C. Percent CO	0 %
7. Area of Stack (As)	0.601 ft ²
8. Pitot Tube Factor (Cp)	0.99

STACK GAS VELOCITY (Vs)	133.79 ft/sec
STACK GAS VOLUMETRIC FLOWRATE (Qs)	1,212 SDCFM
STACK GAS VOLUMETRIC FLOWRATE (Qa)	4,825 ACFM

Vs = velocity of the stack gas (ft/sec)

Qs = Volumetric flowrate at standard conditions

MWs = Mol.Wt.Stack Gas wet

MWd = Mol. Wt. Stack Gas dry

Ps = stack pressure

Delta P = differential pressure measured by the pitot

Calculations,

$$MWs = MWd \times (1 - Bwo) + 18 (Bwo)$$

$$MWd = .44 (\%CO_2) + .32 (\%O_2) + .28 (\%CO + \%N_2)$$

$$Ps = \text{static} / 13.6 + Pb$$

$$Vs = 85.49 \times (Cp) \times \sqrt{P \times (Ts + 460) / (Ps \times MWs)}$$

$$Qs = 1058.8 (1 - Bwo) \times Vs \times As \times Ps / (Ts + 460)$$

$$Qa = 60 \times Vs \times As$$

BEST ENVIRONMENTAL
MOISTURE DETERMINATION

LAIDLAW
Engine #1

Date: 9-22-92
Method: CARB M4
Time: 0925-0955
Fuel: Landfill Gas
RUN#: 1

1. Uncorrected Meter Volume (Vm)	17.691 ft3
2. Meter Factor (Yd)	0.9912
3. Barometric Pressure (Pb)	29.98 Hg
4. Meter Pressure (PH)	0.2 H2O
5. Meter Temperature (Tm)	75.4 F
6. Std. Temperature (Tstd)	70.0 F
7. Impinger H2O Gain (Vw)	72.0 ml
8. Silica Gel Wt. Gain (Vw)	6.5 gm
9. Moisture Vapor (Vw std)	3.71 ft3
Std. Meter Volume (Vm std)	17.402 ft3
Percent of H2O in Stack (% H2O)	17.58 %

ft3 = Cubic Feet
Hg = Mercury
F = Fahrenheit
ml = milliliters
gm = grams
% = Percent

Calculations,

Moisture Vapor = $0.00267 \times \text{ml cond.} \times 460 + \text{Std Temp.} / 29.92$
Std Meter Vol = $\text{Vm} \times \text{Yd} \times \text{Tstd} + 460 \times \text{Pb} + \text{PH} / \text{Tm} + 460 \times 29.92$
Stack Moisture = $\text{Moisture Vapor} / \text{Moisture Vapor} + \text{Std. Vol.}$

STACK VOLUMETRIC FLOWRATE DETERMINATION

Date 9-22-92 Client Laidlaw/Newby Is. #1 Operators DC/JM
Time 10:10 A.M. Barometric (Pb) _____ Static _____
Location Eng #1 Pressure 29.98 Pressure + 4.0
Pitot Factor .99 Duct dimen. 10.5" ID. _____
CO2% 17.0 Stack Area (As) .601
O2% 0.6 Round duct = $\pi r^2 \div 144$ (radius in inches)
H2O% _____

Velocity Traverse Data

Remarks

Inches from wall	Port &pt.	Time	Delta P	Stack Temp	sqr.t. ⁻ P
			7		
		1010	1.25	1294	
			1.30		
			1.15		
			1.10		
			1.10		
			1.5		(1.109)
Averages					

Stack Gas Velocity
@ Stack conditions
(feet per second)

$$V_s = 85.49 \times (C_p) \times \sqrt{p_{avg.} \times \sqrt{[T_{savg} \times 460 / P_{sx} M W_s]}}$$

Where,

Vs=velocity stack

C_p = pitot factor

Ts=Stack Temperature

Ps=Stack pressure

MWs=Molecular Wt.gas

where,

$$MWS = MWD \times (1 - BWO) + 18 (BWO)$$

$$MWd = .44 (\%CO_2) + .32 (\%O_2) + .28 (\%CO + \%N_2)$$

$$Bwo = \%moisture / 100$$

$$P_s = \text{static} / 13.6 + P_b$$

Stack Gas Volume at Standard Conditions

Qs = SCFM

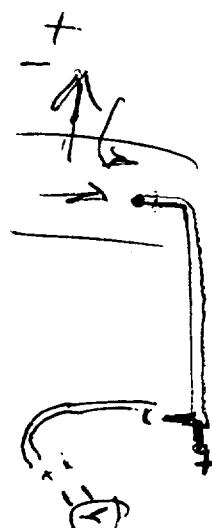
$$Q_s = 60(1 - B_{wo}) \times V_{savg} \times A_s \times (528 / T_{savg} + 460) \times (P_s / 29.92)$$

$V_S =$ _____

Qs= _____

Averages.

Notes/Comments



BEST ENVIRONMENTAL Particulate Field Data Sheet

Run # 1 Method # 4

LAIDLAW

Plant NEWBY ISLAND
 Date 9-22
 Location ENGINE # 1
 Port Dia. _____
 Stack I.D. 10.5"
 Stack Area _____ ft²
 Personnel DC/Jm

OH# 2.383 XH₂O Assum. _____ Filter # _____
 Meter Yd 09912 Pitot Cp _____ Pitot # _____
 PBar. 29.98 Noz. Diam. _____ Net Imp Vol 72
 Stat Press _____ Noz. I.D. _____ Tot Imp Vol 272
 X_{CO2} Assum _____ Meter # 8812 Sample Time 30
 X_{CO2} Assum _____ Probe # _____ Sqrt ΔP Ave _____
 Pre leak ck .002 cfm 15 "Hg Post leak ck .601 cfm 5 "Hg
 F.H. Wt. (mg) _____
 S.H. Wt. (mg) _____
 Gel Wt. (mg) 6.5
 X_{CO2} Actual _____
 X_{CO2} Actual _____
 Tot. Moisture _____
 Std Vm _____

Sample Point	Clock Time	Vel. ΔP	M.R. cfm	Drif. ΔH	Gas Meter Volume ft ²	Gas Meter In	Gas Meter Out	Temperatures F				Pump Vac.	Comments
1					<u>477.966</u>	<u>71</u>	<u>70</u>					<u>4</u>	
2	<u>9:25</u>				<u>480.029</u>	<u>71</u>	<u>70</u>	<u>1294°</u>				<u>4</u>	
3	<u>30</u>				<u>483.050</u>	<u>75</u>	<u>71</u>						
4	<u>35</u>				<u>485.990</u>	<u>77</u>	<u>72</u>						
5	<u>40</u>				<u>483.920</u>	<u>79</u>	<u>72</u>						
6	<u>45</u>				<u>491.855</u>	<u>80</u>	<u>73</u>						
7	<u>50</u>				<u>494.790</u>	<u>82</u>	<u>74</u>						
8	<u>9:55</u>				<u>497.720</u>	<u>84</u>	<u>75</u>					<u>4</u>	
9													
10					<u><17.691></u>		<u><75.7></u>						
11													
12													
13													
14													
15													
16													
17													
18													
19													
20													
21													
22													
23													
24													
25													
26													
27													
28	Average												

Notes:

Ms =
 Ave. Vs =
 Sample I.D. # =

Final Imp Vol = 177
 Initial Imp Vol = 102

BEST ENVIRONMENTAL
Stack Gas Volumetric Flowrate Determination

Client: <u>Laidlaw</u>					Location: <u>Newby Island Eng #2</u>				
Date: <u>10/9/92</u> Time: <u>1305</u>					Run#: <u>1</u>				
Pitot Factor (Cp): <u>.89</u>					Operators: <u>DC/SM</u>				
Assumed %O2: Actual <u>1.5</u>					Barometric (Pb): <u>29.95</u> $P_s = 30.28$				
Assumed %CO2: Actual <u>17.4</u>					Static Pressure (Pstatic): <u>+ 4.5</u>				
Assumed %CO: Actual					Stack Diameter, in: <u>10.5</u>				
Assumed %H2O: Actual <u>16.6</u>					Stack Area, ft² (As): <u>.601</u>				
Port ID & Point#	Point Location, inches	Delta P, (inches Hg)	Stack Temp °F, (ts)	.SQRT -P	CALCULATIONS				
		<u>.9</u>	<u>1160</u>		<u>Stack Gas Velocity, actual feet per sec (Vs)</u> $V_s = 85.49 \cdot C_p \cdot (\text{SQRT } P_{\text{avg}} \cdot \text{SQRT} [(ts + 460)/P_s \cdot MW_s])$ $V_s = \underline{116.9}$				
		<u>1.1</u>	<u>↓</u>						
		<u>1.1</u>	<u>↓</u>						
		<u>1.0</u>	<u>↓</u>						
				<u><1.012</u>	<u>Molecular Weight of Stack Gas, g/g.mole (MWs)</u> $MW_s = MW_d \cdot (1 - B_{wo}) + 18(B_{wo})$ $MW_s = \underline{28.71}$				
					<u>Molecular Weight of Dry Gas, g/g.mole (MWd)</u> $MW_d = 0.44(\%CO_2) + 0.32(\%O_2) + 0.28(\%CO + N_2)$ $MW_d =$				
					<u>Stack Gas Volumetric Flow Rate, standard dry cubic feet/min (SDCFM)</u> $SDCFM = 60(1 - B_{wo}) \cdot V_s \cdot A_s \cdot 528 / [(ts + 460) \cdot P_s / 29.92]$ $SDCFM = \underline{1160}$				
					WHERE:				
					<u>Stack Pressure, in Hg (Ps)</u> $P_s = P_b + (P_{\text{static}}/13.6)$				
					<u>Water Vapor Fraction, (Bwo)</u> $B_{wo} = \%H_2O/100$				
					<u>Stack Area, ft² (As)</u> $A_s = (\text{Diameter}/24)^2 \cdot 3.1416$				
					Comments:				
AVG									

BEST ENVIRONMENTAL Particulate Field Data Sheet

Run # 1 Method # 4

Plant L AID LAW
 Date 10-9
 Location BOILER #2
 Port Dia. _____
 Stack I.D. _____
 Stack Area _____ ft²
 Personnel DC/Jm

Alt 2.383
 Meter Yd 0.9912
 PBar. 29.95
 Stat Press _____
 XCO₂ Assum _____
 XCO₂ Assum _____
 Pre leak ck 0.02 cfm

XH₂O Assum. _____
 Pitot Cp _____
 Noz. Diam. _____
 Noz I.D. _____
 Meter # 8812
 Probe # _____

Filter # _____
 Pitot # _____
 Net Imp Vol 47
 Tot Imp Vol 247
 Sample Time 30
 Sort ΔP Ave _____

F.H. Wt. (mg) _____
 E.H. Wt. (mg) _____
 Gel Wt. (mg) _____
 XCO₂ Actual _____
 XCO₂ Actual _____
 Tot. Moisture _____
 Std Vm 17.242

16.6% H₂O

Sample Point	Clock Time	Vel. ΔP	M.R. cfm	Orif. ΔH	Gas Meter Volume ft ²	Gas Meter		Temperatures F				Pump Vac.	Comments
						In	Out	Stack	Imp.	Filter	Probe		
1	11:51			13	551.450	110	109					2.5	
2	56				534.825	110	115						
3	12:01				557.925	110	116						
4	:04				561.020	111	117						
5	:11				564.110	114	118						
6	:16				567.230	114	118						
7	12:21				570.358	113	118					2.5	
8													
9					18.908		115						
10													
11													
12													
13													
14													
15													
16													
17													
18													
19													
20													
21													
22													
23													
24													
25													
26													
27													
28	Average												

Notes:

$$\text{ml H}_2\text{O} + \text{gel} \times .473 = \text{H}_2\text{O} \text{ g ft}^3$$

Ms =
 Ave. Vs =
 Sample I.B. # =

$$100 \times \frac{\text{ft}^3 \text{H}_2\text{O}}{\text{H}_2\text{O ft}^3 + \text{std Vol}} = \% \text{H}_2\text{O}$$

Final Imp Vol = 61 82
 Initial Imp Vol = 163 104

**BEST ENVIRONMENTAL
CONTINUOUS MONITOR DATA SHEET**

Plant Laidlaw / Newby I.s. #1

Date 9-22-93

Test Location Eng #1

Run Number R-1, 2

Operator DC

Ambient Temperature 75

Barometric Pressure 29.98

Static Pressure Duct +4.0

Fuel Landfill gas

Number _____

Time	Sample Point	Fuel Flow	Dry Uncorrected					3% O ₂ Dry		Hydrocarbons			TOC ppm	CO ₂ ppm	VOC ppm	Comments
			O ₂ %	CO ₂ %	CO ppm	SO ₂ ppm	NO ppm	NO _x ppm	ppm	THC	CH ₄	CH ₄				
			8.65	13.38	25.7			199.9		1776						900 RPM
										84.6						450 KW
926			0.6	17.0	1.0			275		1840	<25					
936			0.6	17.0	1.0			280		2000	<25					
946			0.6	17.1	1.0			280		2000	<25					
956	zero		0.6	17.1	1.0			280		0						
	cal		8.65	12.5	81			200		1750						
	Ave	→	(0.6)	(17.0)	(1.0)			(178)								
1002			0.6	17.0	1.0			180		1700	<25					
1012			.6	17.0	1.0			190		1630	<25					
1022			.6	17.0	1.0			190		1680	<25					
1032	zero		0.6	17.0	1.0			0		0						
	cal		8.6	12.2	81			200		1780						
	Ave	→	(0.6)	(17.0)	(1.0)			(187)		(1688)						
1038			0.6	17.3	1.0			190		1650	<25					
1048			0.7	17.3	1.0			190		1660	<25					
1058			0.6	17.2	1.0			185		1640	<25					
1108	zero		0.6	17.2	1.0			0		0						
	cal		8.7	12.5	81			200		1770						
	Ave	→	(0.6)	(17.2)	(1.0)			(188)		(1657)						

Plant Laidlaw
Date 10-9-92
Test Location Newby Is. Eng #2
Run Number 1,2,3
Operator DC

Ambient Temperature 72
Barometric Pressure 29.95
Static Pressure Duct _____
Fuel Landfill Gas
Number _____

Time	Sample Point	Fuel Flow	Dry Uncorrected						3% O ₂ Dry		Hydrocarbons			TOC ppm	CO ₂ ppm	VOC ppm	Comments
			O ₂ %	CO ₂ %	CO ppm	SO ₂ ppm	NO ppm	NO _x ppm	ppm	NO _x ppm	THC	CH ₄	Non CH ₄				
Span	Cal		8.54	11.85	916				938			84.6					
1142			1.5	17.2	1150				520			24	24	<5			
1157			1.5	17.2	1140				500			25	25	<5			
1213			1.5	17.2	1135				540			25	25	<5			
	zero		0	0	0				0			0	0	0			
	cal		8.5	11.9	890				930			89					
	Ave		1.5	17.2	1138				520			25		<5			
1220			1.4	17.3	1125				500			25	25	<5			
1235			1.4	17.4	1000				470			25	25	<5			
1250			1.4	17.4	1010				470			25	25	<5			
	zero		0	0	0				0			0	0	0			
	cal		8.75	11.8	920				932			84					
	Ave		1.4	17.4	1045				480			25		<5			
1254			1.5	17.4	1100				500			35					
1309			1.5	17.4	1050				500			25					
1324			1.5	17.4	1075				500			25					
	zero		0	0	0				0			0	0	0			
	cal		8.9	11.8	890				934			82					
	Ave		1.5	17.4	1075				500			25					

Eng #1 R-3

1038

CO₂ 0-25%

9/22/92

NO_x 0-1000 ppm
D-1000

1001

941

Eng #1 R-1

CO₂ 0-25%
926

NO_x 0-1000 ppm

9/22/92

1 idler, Hawley Jr.

1330 - 1282

1215

102-0-25%

1150

1145

Newby Is. #1

102-0-25%

9/22/92

43
R-2

NOx
0-1000

NOx
0-1000 ppm

Eng #3
R-1

R-3

#1

Eng #1 R-3

1098

Eng #1 R-2
9-22-92

09-10-10

0-10-10

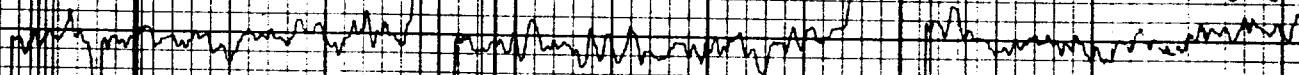
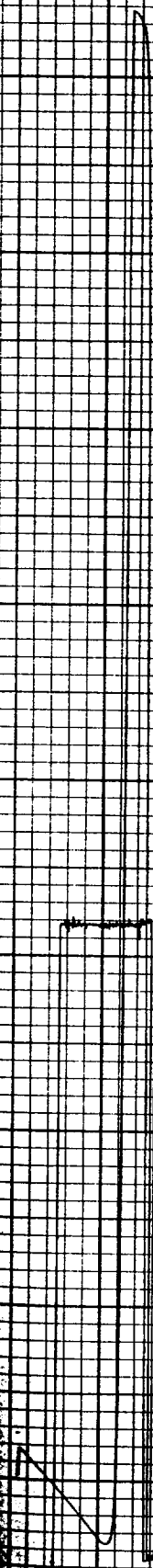
1002

Eng #1 R-1

02-0-20%

926

1-11-92, Newby Is. 9-22-92



0-2500 ppm

0-10%

1 cal

5-1303

200

Landline
Newly Island
Aug 82

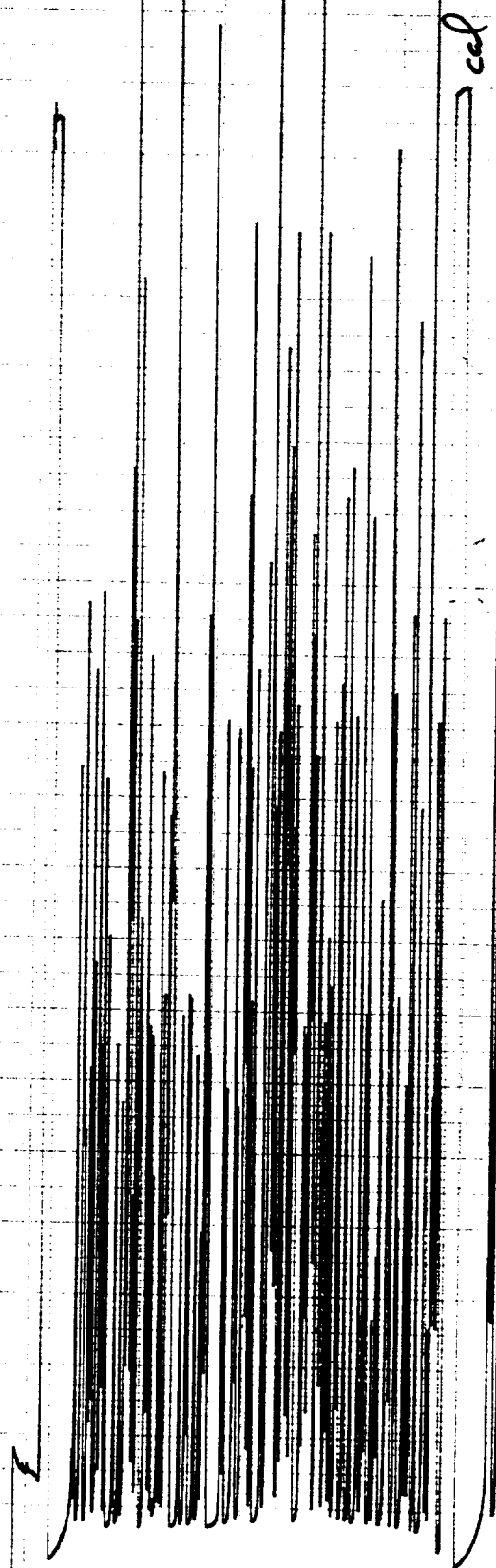
Run 1

0-10%

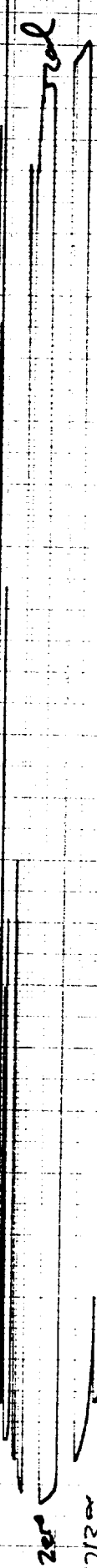
0-1500 ppm

0-2500 ppm

5-142



Run 2
THC 0-100 ppm



Run 1 Laidlaw
Newby Island
Eng #2

THC 0-300 ppm
- 0-100 ppm

Ballantyne Island
Newby #2
Eng
10/9/92





SCOTT-MARRIN, INC.

2001 THIRD ST. • UNIT H • RIVERSIDE, CA 92507
TELEPHONE (714) 784-1240

REPORT OF ANALYSIS
NIST TRACEABLE GAS MIXTURES

BEST01
TO: REGAN BEST
BEST ENVIRONMENTAL
27343 INDUSTRIAL BLVD.
SUITE E
HAYWARD, CA 94545

DATE: 05/31/91

CUSTOMER ORDER NUMBER: 8289

PAGE 1

CYLINDER NUMBER	COMPONENT	CONCENTRATION(v/v)	NIST TRACEABLE REFERENCE STANDARD
CC12793	Nitric Oxide Nitrogen, O ₂ -Free	199.9 ± 4.0 ppm Balance	SRM 1685b

ppm = umole/mole

% = mole-%

The above analysis is traceable to the National Institute of Standards and Technology by intercomparison with the reference standard listed above. Where indicated, volumetric and gravimetric reference standards are traceable thru use of our analytical balance. NIST Report No. MMAP 232.09/202491.

Analyst:

B.E. Gross

Approved:

J.T. Marrin

The only liability of this company for gas which fails to comply with this analysis shall be replacement or reanalysis thereof by the company without extra cost.

STANDARD CALIBRATION GASES IN ALUMINUM CYLINDERS



6531 BOX SPRINGS BLVD. • RIVERSIDE, CA 92507
TELEPHONE (714) 653-6780 • FAX (714) 653-2430

REPORT OF ANALYSIS
NIST TRACEABLE GAS MIXTURES

TO:

Craig Thiry
Best Environmental
15890 Foothill Blvd.
San Leandro, CA 94578-2101

DATE: 04/02/92

CUSTOMER ORDER NUMBER: 8416

PAGE 1

CYLINDER NUMBER	COMPONENT	CONCENTRATION (v/v)	NIST TRACEABLE REFERENCE STANDARD
CC12567	Propane Zero Air	592 ± 6 ppm Balance	SRM 2646

$$\text{ppm} = \text{umole/mole}$$

$\% = \text{mole-}\%$

The above analysis is traceable to the National Institute of Standards and Technology by intercomparison with the reference standard listed above. Where indicated, volumetric and gravimetric reference standards are traceable thru use of our analytical balance. NIST Report No. MMAP 232.09/202491.

Analyst:

M.S. Calhoun

Approved:

J.T. Marrin

The only liability of this company for gas which fails to comply with this analysis shall be replacement or reanalysis thereof by the company without extra cost.

STANDARD CALIBRATION GASES IN ALUMINUM CYLINDERS



SCOTT-MARRIN, INC.

6531 BOX SPRINGS BLVD • RIVERSIDE, CA 92507
TELEPHONE (714) 653-6780 • FAX (714) 653-2430

REPORT OF ANALYSIS NIST TRACEABLE GAS MIXTURES

BEST01

TO:

CRAIG THIRY
BEST ENVIRONMENTAL
15890 FOOTHILL BLVD.
SAN LEANDRO, CA 94578-2101

DATE: 08/06/92

CUSTOMER ORDER NUMBER: 8446

PAGE 1

CYLINDER NUMBER	COMPONENT	CONCENTRATION (v/v)	NIST TRACEABLE REFERENCE STANDARD
CC114767	Carbon Monoxide	80.0 ± 0.8 ppm	SRM 1679c
	Carbon Dioxide	12.38 ± 0.12 %	SRM 1675b
	Oxygen	8.68 ± 0.09 %	SRM 2658a
	Nitrogen	Balance	

ppm = umole/mole

% = mole-%

The above analyses are traceable to the National Institute of Standards and Technology by intercomparison with the reference standards listed above. Where indicated, volumetric and gravimetric reference standards are traceable thru use of our analytical balance. NIST Report No. MMAP 232.09/207491.

Analyst:

M.S. Calhoun

M.S. Calhoun

Approved:

J.T. Marrin

J.T. Marrin

The only liability of this company for gas which fails to comply with this analysis shall be replacement or reanalysis thereof by the company without extra cost.

STANDARD CALIBRATION GASES IN ALUMINUM CYLINDERS