

Note: This is a reference cited in AP 42, *Compilation of Air Pollutant Emission Factors, Volume I Stationary Point and Area Sources*. AP42 is located on the EPA web site at www.epa.gov/ttn/chiefl/ap42/

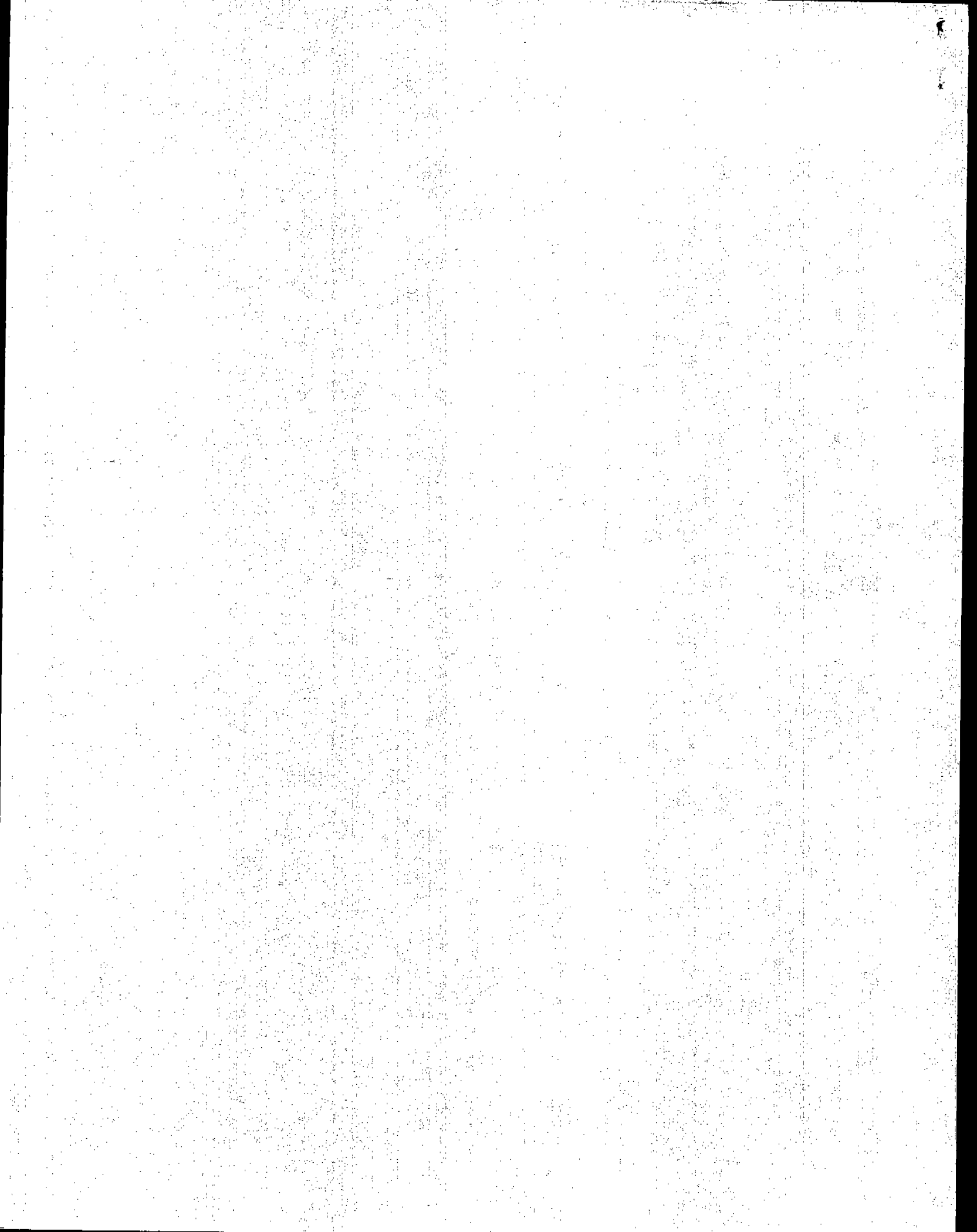
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FINAL REPORT FOR EMISSIONS COMPLIANCE TESTING OF ONE WAUKESHA ENGINE GENERATOR

Browning Ferris Gas Services, Inc.
Chicopee, MA

February 1994

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**FINAL REPORT FOR EMISSIONS COMPLIANCE
TESTING OF ONE WAUKESHA ENGINE GENERATOR**

Prepared for

Browning-Ferris Gas Services, Inc.
Chicopee, MA

(TRC Ref. 15147-0010-00000)

February 1994

TRC ENVIRONMENTAL CORPORATION

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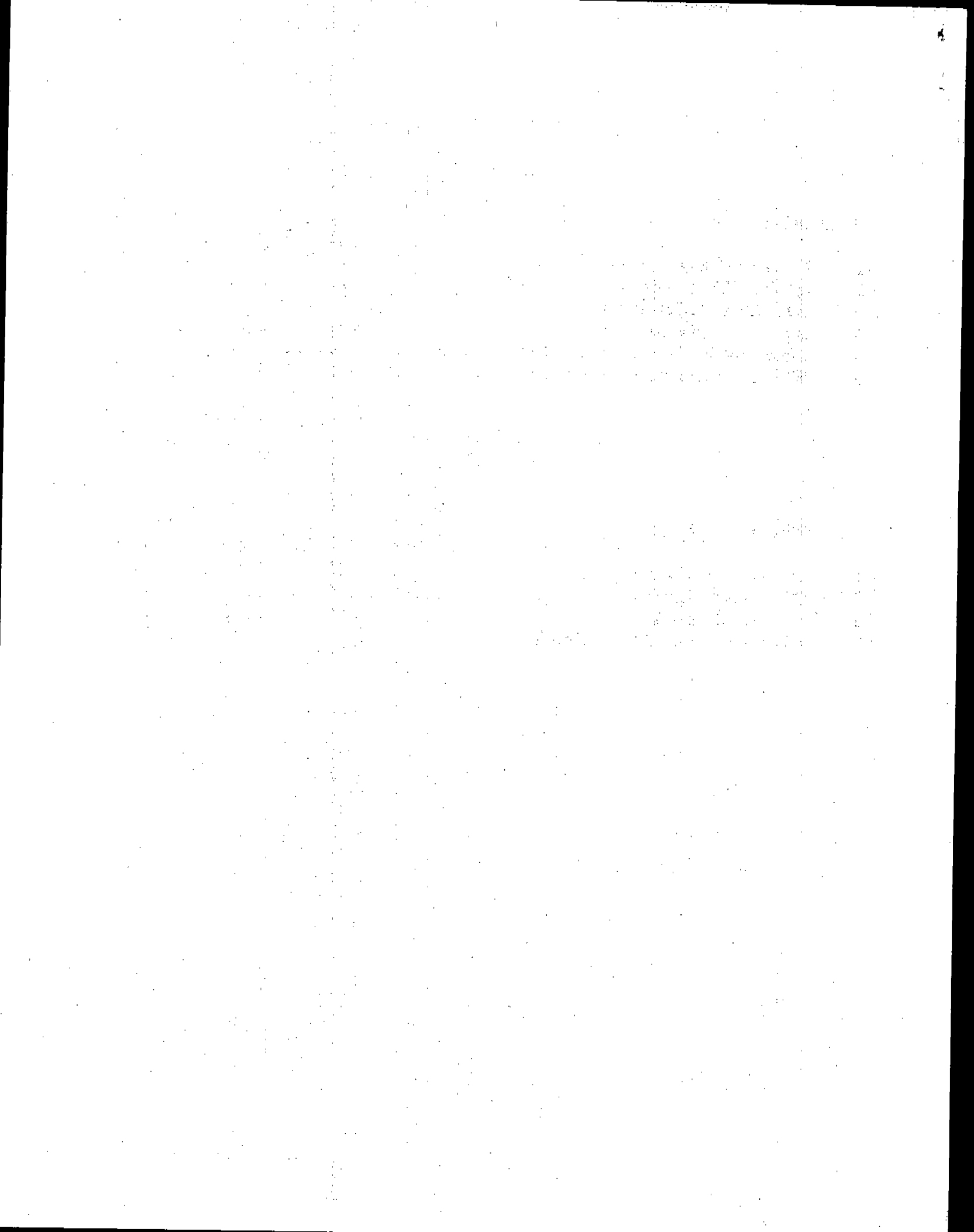
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SECTION 1

INTRODUCTION

1.1 OVERVIEW

TRC Environmental Corporation, under contract to Browning-Ferris Gas Services, Inc., (BFGSI) conducted an emissions compliance test program on one Waukesha engine generator on December 14, 1993. The engine generator is located at BFGSI's Chicopee, Massachusetts facility. This compliance test program determined the gaseous pollutant and visible emission rates from the engine generator. All compliance testing was conducted in accordance with 40 CFR 60 Appendix A reference methods.

1.2 REPORT SUMMARY

This report presents the results of the test program completed at BFGSI's Chicopee facility. Included in the following pages are descriptions of the sampling location, sampling and analytical procedures, and TRC's QA procedures which ensure the integrity of the reported data. A summary of all test results is presented in Section 2. Additionally, appendices are included which contain all relevant field sampling data sheets, continuous emissions monitoring data sheets, gas chromatograph data sheets, visible emission observation data and certification sheet, and facility process data.

SECTION 2

SUMMARY OF RESULTS

This section presents a summary of the emission testing results on the Waukesha engine generator. The field sampling data sheets are located in Appendix A. Continuous emissions monitoring data can be found in Appendix B. Gas chromatograph data is located in Appendix C. The visible observation data and certification sheet can be found in Appendix D. The facility process data can be found in Appendix E. Calibration data sheets can be found in Appendix F.

2.1 WAUKESHA ENGINE EMISSIONS RESULTS

Three 60-minute test runs were conducted at the outlet stack on the Waukesha engine generator. This engine is designed to produce 1025 Kilowatts per hour (KW/hr). The emission results for NO_x , CO, SO_2 , and TGNMO for the three test runs are presented in terms of parts per million (ppm), pounds per hour (lbs/hr), and grams per horse power hour (gm/HP-hr). These results are presented Table 2-1. Sampling parameters and flow rates obtained during each test run are presented in Table 2-2. The emission limits stated in the permit were met. The field data sheets can be found in Appendix A. The continuous emissions monitoring data can be found in Appendix B and the gas chromatograph data can be found in Appendix C.

2.2 VISIBLE EMISSIONS RESULTS

Three 60-minute visible emissions observation test runs were conducted December 14, 1993 on the engine generator. Readings were obtained from the flue gas exiting the stack. The overall percent opacity for the engine generator was 0. Table 2-3 presents the average opacity recorded during each observation test run. Tables 2-4 through 2-6 presents the visible emissions data summary for each run. The field data recordings and certification sheet can be found in Appendix D.

TABLE 1-1. BFI CHICOPEE ENGINE EMISSIONS AVERAGES

PARAMETER	EXHAUST GAS FLOW RATE (dscfm)	NO _x (ppm)	CO (ppm)	THC (ppm)	METHANE (ppm)	TGNMO (ppm)	SO ₂ (ppm)	EMISSION (lb/hr)				EMISSION (gm/HP-hr)				EMISSION (tons/year)*			
								NO _x	CO	TGNMO	SO ₂	NO _x	CO	TGNMO	SO ₂	NO _x	CO	TGNMO	SO ₂
Landfill Gas Average Run 1	3,257	78.01	447.84	2120.53	2044.9	75.6	0.00	1.82	6.36	0.61	0.00	0.30	1.05	0.10	0.00	7.97	27.86	2.69	0.00
Landfill Gas Average Run 2	3,274	74.40	447.01	2146.28	2034.5	91.8	0.00	1.74	6.38	0.75	0.00	0.29	1.05	0.12	0.00	7.64	27.95	3.28	0.00
Landfill Gas Average Run 3	3,286	65.96	437.14	2156.12	1994.6	161.5	1.10	1.55	6.26	1.32	0.04	0.26	1.03	0.22	0.00	6.80	27.43	5.79	0.16
AVERAGE	3,272	72.79	444.06	2140.98	2031.3	109.6	0.37	1.71	6.33	0.89	0.01	0.28	1.04	0.15	0.00	7.47	27.75	3.92	0.65

* - Tons/year based on 365 days/year, 24 hours/day

ENGINE EMISSION LIMITS

PARAMETER	EMISSION (lb/hr)				EMISSION (gm/HP-hr)				EMISSION (tons/year)			
	NO _x	CO	TGNMO	SO ₂	NO _x	CO	TGNMO	SO ₂	NO _x	CO	TGNMO	SO ₂
Landfill Gas	8.8	21.9	2.4	1.6	0.9	2.25	0.25	0.00	38.0	96.00	11.00	7.00

Fuel flow avg = 22.017 MM BTU/HR (avg from 2 runs)

$$NO_x EF = \frac{1.71 \text{ lb/hr}}{22.017 \text{ MM BTU/HR}} = 7.77 \times 10^{-2} \text{ lb/MM BTU}$$

$$CO EF = \frac{6.33 \text{ lb/hr}}{22.017 \text{ MM BTU/HR}} = 2.88 \times 10^{-1} \text{ lb/MM BTU}$$

TABLE 2-2. BFI - CHICOPEE
METHOD 4/CEM SAMPLING PARAMETERS - RUNS 1-3

Run No.	1	2	3	
Date	14-Dec-93	14-Dec-93	14-Dec-93	
Start Time	11:49	13:42	15:30	
Stop Time	12:49	14:42	16:30	AVERAGES
Barometric Pressure, in. Hg	29.39	29.39	29.39	29.39
Net Sampling Time, minutes	30.0	30.0	30.0	30.0
Volume Metered, cf	22.115	22.361	22.528	22.335
Avg. DGM Temp, F	95	100	100	98
AVG Delta H, in of H2O	2.0	2.0	2.0	2.0
AVG Delta H, in of Hg	0.1471	0.1460	0.1471	0.1467
DGM Calibration Factor	0.980	0.980	0.980	0.980
Volume of Gas Collected, dscf	20.344	20.407	20.555	20.435
Total Water Collected, mL	51.6	54.4	57.5	54.5
Volume of Water Vapor, scf	2.433	2.565	2.711	2.570
Moisture, %	10.7	11.2	11.7	11.2
Dry Mole Fraction, 100-%M	0.8932	0.8883	0.8835	0.8883
CO2 at Stack, % dry	11.00	11.08	10.97	11.02
O2 at Stack, % dry	8.94	9.16	9.33	9.14
CO + N2, % dry	80.06	79.76	79.70	79.84
Dry Molecular Weight, lb/lb mole	30.12	30.14	30.13	30.13
Wet Molecular Weight, lb/lb mole	28.82	28.78	28.72	28.77
Excess Air at Stack, %	73.3	77.0	79.7	76.7
Stack Area, sq. in. (14-in ID)	153.9	153.9	153.9	153.9
Static Pressure, in. of H2O	1.50	2.00	2.25	1.92
Stack Pressure, in. of Hg	29.50	29.54	29.56	29.53
Avg. Stack Temp., F	710	711	708	710
Avg. Sqrroot of Delta P	1.5167	1.5316	1.5411	1.5298
SDE Average	51.887	52.408	52.672	52.322
Pitot Coefficient	0.84	0.84	0.84	0.84
Stack Gas Velocity, afpm	7,668	7,745	7,791	7,735
Stack Flowrate, wet acfm	8,197	8,280	8,329	8,268
Stack Flowrate, dry scfm	3,257	3,274	3,286	3,272

BFI-1-3.mt1

TABLE 2-3
VISIBLE EMISSION TEST RESULTS

Date	Run No.	Time Period	Process	% Opacity Run Averages
12/14/93	1	11:00 to 12:00	Engine Generator	0
12/14/93	2	12:00 to 13:00	Engine Generator	0
12/14/93	3	13:00 to 14:00	Engine Generator	0

Overall % Opacity: 0

BPCVERE.WK1

TABLE 2-4. VISIBLE EMISSION DATA SUMMARY - RUN 1

Company: Browning-Ferris Gas Services, Inc.
Facility: Chicopee, MA

Date: 12/14/93

Run: 1

Process: Landfill Gas Engine Generator

Observer: Timothy J. Sanger

Start Time: 11:00

Stop Time: 11:30

Set No.	Reading Interval				1-min avgs.	6-min avgs.	Rolling 6-min avgs.	Comments
	0 sec.	15 sec.	30 sec.	45 sec.				
1	0	0	0	0	0			
2	0	0	0	0	0			
3	0	0	0	0	0			
4	0	0	0	0	0			
5	0	0	0	0	0			
6	0	0	0	0	0	0	0	
7	0	0	0	0	0		0	
8	0	0	0	0	0		0	
9	0	0	0	0	0		0	
10	0	0	0	0	0		0	
11	0	0	0	0	0		0	
12	0	0	0	0	0		0	
13	0	0	0	0	0	0	0	
14	0	0	0	0	0		0	
15	0	0	0	0	0		0	
16	0	0	0	0	0		0	
17	0	0	0	0	0		0	
18	0	0	0	0	0		0	
19	0	0	0	0	0	0	0	
20	0	0	0	0	0		0	
21	0	0	0	0	0		0	
22	0	0	0	0	0		0	
23	0	0	0	0	0		0	
24	0	0	0	0	0	0	0	
25	0	0	0	0	0		0	
26	0	0	0	0	0		0	
27	0	0	0	0	0		0	
28	0	0	0	0	0		0	
29	0	0	0	0	0		0	
30	0	0	0	0	0	0	0	

30 Minute Average:

0 % Opacity

BFC-VET 1001

TABLE 2-4. VISIBLE EMISSION DATA SUMMARY - RUN 1 (continued)

Company: Browning-Ferris Gas Services, Inc.
Facility: Chicopee, MA

Date: 12/14/93

Process: Landfill Gas Engine Generator

Run: 1

Start Time: 11:30

Observer: Timothy J. Senger

Stop Time: 12:00

Set No.	Reading Interval				1-min avg.	5-min avg.	Rolling 5-min avg.	Comments
	0 sec.	15 sec.	30 sec.	45 sec.				
1	0	0	0	0	0			
2	0	0	0	0	0			
3	0	0	0	0	0			
4	0	0	0	0	0			
5	0	0	0	0	0			
6	0	0	0	0	0	0	0	
7	0	0	0	0	0		0	
8	0	0	0	0	0		0	
9	0	0	0	0	0		0	
10	0	0	0	0	0		0	
11	0	0	0	0	0		0	
12	0	0	0	0	0	0	0	
13	0	0	0	0	0		0	
14	0	0	0	0	0		0	
15	0	0	0	0	0		0	
16	0	0	0	0	0		0	
17	0	0	0	0	0		0	
18	0	0	0	0	0	0	0	
19	0	0	0	0	0		0	
20	0	0	0	0	0		0	
21	0	0	0	0	0		0	
22	0	0	0	0	0		0	
23	0	0	0	0	0		0	
24	0	0	0	0	0	0	0	
25	0	0	0	0	0		0	
26	0	0	0	0	0		0	
27	0	0	0	0	0		0	
28	0	0	0	0	0		0	
29	0	0	0	0	0		0	
30	0	0	0	0	0	0	0	

8FIC-VET MKT

30 Minute Average:

0 % Opacity

Run Average:

0 % Opacity

TABLE 2-5. VISIBLE EMISSION DATA SUMMARY -- RUN 2

Company: Browning-Ferris Gas Services, Inc.
 Facility: Chicopee, MA

Date: 12/14/83

Run: 2

Process: Landfill Gas Engine Generator

Observer: Timothy J. Senger

Start Time: 12:00

Stop Time: 12:30

Set No.	Reading Interval				1-min avg.	6-min avg.	Rolling 6-min avg.	Comments
	0 sec.	15 sec.	30 sec.	45 sec.				
1	0	0	0	0	0			
2	0	0	0	0	0			
3	0	0	0	0	0			
4	0	0	0	0	0			
5	0	0	0	0	0			
6	0	0	0	0	0	0	0	
7	0	0	0	0	0		0	
8	0	0	0	0	0		0	
9	0	0	0	0	0		0	
10	0	0	0	0	0		0	
11	0	0	0	0	0		0	
12	0	0	0	0	0	0	0	
13	0	0	0	0	0		0	
14	0	0	0	0	0		0	
15	0	0	0	0	0		0	
16	0	0	0	0	0		0	
17	0	0	0	0	0		0	
18	0	0	0	0	0	0	0	
19	0	0	0	0	0		0	
20	0	0	0	0	0		0	
21	0	0	0	0	0		0	
22	0	0	0	0	0		0	
23	0	0	0	0	0		0	
24	0	0	0	0	0	0	0	
25	0	0	0	0	0		0	
26	0	0	0	0	0		0	
27	0	0	0	0	0		0	
28	0	0	0	0	0		0	
29	0	0	0	0	0		0	
30	0	0	0	0	0	0	0	

30 Minute Average:

0 % Opacity

BFC-VET.WK1

TABLE 2-5. VISIBLE EMISSION DATA SUMMARY - RUN 2 (continued)

Company: Browning-Ferris Gas Services, Inc.
 Facility: Chicopee, MA

Date: 12/14/93

Process: Landfill Gas Engine Generator

Run: 2

Start Time: 12:30

Observer: Timothy J. Senger

Stop Time: 13:00

Set No.	Reading Interval				1-min avgs.	5-min avgs.	Rolling 5-min avgs.	Comments
	0 sec.	15 sec.	30 sec.	45 sec.				
1	0	0	0	0	0			
2	0	0	0	0	0			
3	0	0	0	0	0			
4	0	0	0	0	0			
5	0	0	0	0	0			
6	0	0	0	0	0	0	0	
7	0	0	0	0	0		0	
8	0	0	0	0	0		0	
9	0	0	0	0	0		0	
10	0	0	0	0	0		0	
11	0	0	0	0	0		0	
12	0	0	0	0	0	0	0	
13	0	0	0	0	0		0	
14	0	0	0	0	0		0	
15	0	0	0	0	0		0	
16	0	0	0	0	0		0	
17	0	0	0	0	0		0	
18	0	0	0	0	0	0	0	
19	0	0	0	0	0		0	
20	0	0	0	0	0		0	
21	0	0	0	0	0		0	
22	0	0	0	0	0		0	
23	0	0	0	0	0		0	
24	0	0	0	0	0	0	0	
25	0	0	0	0	0		0	
26	0	0	0	0	0		0	
27	0	0	0	0	0		0	
28	0	0	0	0	0		0	
29	0	0	0	0	0		0	
30	0	0	0	0	0	0	0	

BFG-VET MK7

30 Minute Average:

0 % Opacity

Run Average:

0 % Opacity

TABLE 2-6. VISIBLE EMISSION DATA SUMMARY - RUN 3

Company: Browning-Ferris Gas Services, Inc.
Facility: Chicopee, MA

Date: 12/14/93

Run: 3

Process: Landfill Gas Engine Generator

Observer: Timothy J. Senger

Start Time: 13:00

Stop Time: 13:30

Set No.	Reading Interval				1-min avgs.	6-min avgs.	Rolling 6-min avgs.	Comments
	0 sec.	15 sec.	30 sec.	45 sec.				
1	0	0	0	0	0			
2	0	0	0	0	0			
3	0	0	0	0	0			
4	0	0	0	0	0			
5	0	0	0	0	0			
6	0	0	0	0	0	0	0	
7	0	0	0	0	0		0	
8	0	0	0	0	0		0	
9	0	0	0	0	0		0	
10	0	0	0	0	0		0	
11	0	0	0	0	0		0	
12	0	0	0	0	0	0	0	
13	0	0	0	0	0		0	
14	0	0	0	0	0		0	
15	0	0	0	0	0		0	
16	0	0	0	0	0		0	
17	0	0	0	0	0		0	
18	0	0	0	0	0	0	0	
19	0	0	0	0	0		0	
20	0	0	0	0	0		0	
21	0	0	0	0	0		0	
22	0	0	0	0	0		0	
23	0	0	0	0	0		0	
24	0	0	0	0	0	0	0	
25	0	0	0	0	0		0	
26	0	0	0	0	0		0	
27	0	0	0	0	0		0	
28	0	0	0	0	0		0	
29	0	0	0	0	0		0	
30	0	0	0	0	0	0	0	

30 Minute Average:

0 % Opacity

BPG-VET.WK1

TABLE 2-6. VISIBLE EMISSION DATA SUMMARY - RUN 3 (continued)

Company: Browning-Ferris Gas Services, Inc.
Facility: Chicopee, MA

Date: 12/14/93

Process: Landfill Gas Engine Generator

Run: 3

Start Time: 13:30

Observer: Timothy J. Senger

Stop Time: 14:00

Set No.	Reading Interval				1-min avgs.	6-min avgs.	Rolling 6-min avgs.	Comments
	0 sec.	15 sec.	30 sec.	45 sec.				
1	0	0	0	0	0			
2	0	0	0	0	0			
3	0	0	0	0	0			
4	0	0	0	0	0			
5	0	0	0	0	0			
6	0	0	0	0	0	0	0	
7	0	0	0	0	0		0	
8	0	0	0	0	0		0	
9	0	0	0	0	0		0	
10	0	0	0	0	0		0	
11	0	0	0	0	0		0	
12	0	0	0	0	0	0	0	
13	0	0	0	0	0		0	
14	0	0	0	0	0		0	
15	0	0	0	0	0		0	
16	0	0	0	0	0		0	
17	0	0	0	0	0		0	
18	0	0	0	0	0	0	0	
19	0	0	0	0	0		0	
20	0	0	0	0	0		0	
21	0	0	0	0	0		0	
22	0	0	0	0	0		0	
23	0	0	0	0	0		0	
24	0	0	0	0	0	0	0	
25	0	0	0	0	0		0	
26	0	0	0	0	0		0	
27	0	0	0	0	0		0	
28	0	0	0	0	0		0	
29	0	0	0	0	0		0	
30	0	0	0	0	0	0	0	

30 Minute Average:

0 % Opacity

Run Average:

0 % Opacity

BPC-VET.WKT

SECTION 3

PROCESS DESCRIPTION

The Waukesha engine generator located at BFGSI's Chicopee facility is an industrial engine generator fitted with a Woodward hydraulic governor and utilizes fuel at a rate of 7,350 BTU/hp·hr. The engine will fire 450 SCFM of landfill gas with an average methane content of approximately 44 percent. The engine is rated to produce 985 KW/hr. The gross heating value of methane gas is 909 Btu per cubic foot which will provide for an input rating of 10.8 million Btu per hour. For this test program, the engine generator was at the highest possible load producing 1025 KW/hr. The load obtained during this program was beyond normal operation for the generator. Facility process data can be found in Appendix E.

$$\frac{10.8}{x} = \frac{985}{1025}$$
$$x = 11.24$$

SECTION 4

SAMPLING LOCATION

Sampling of the flue gas emissions were conducted from two 90° sample ports located on the outlet stack of the engine generator. Each of the three test runs were 60 minutes in length consisting of a velocity profile before and after each. Percent moisture was determined for each sample run.

Figure 4-1 presents a schematic diagram of the sampling location of the outlet stack. The outlet stack was 14-inches in diameter which corresponds to an internal stack area of 153.9 in². The matrix of the 8 velocity sampling points within the 14-inch stack, as defined by Method 1. Percent moisture was determined from a single point of average velocity within the flue gas. Flue gas emissions for NO_x, CO, SO₂, TGNMO, O₂ and CO₂ were determined from a three point traverse across the sample plane.

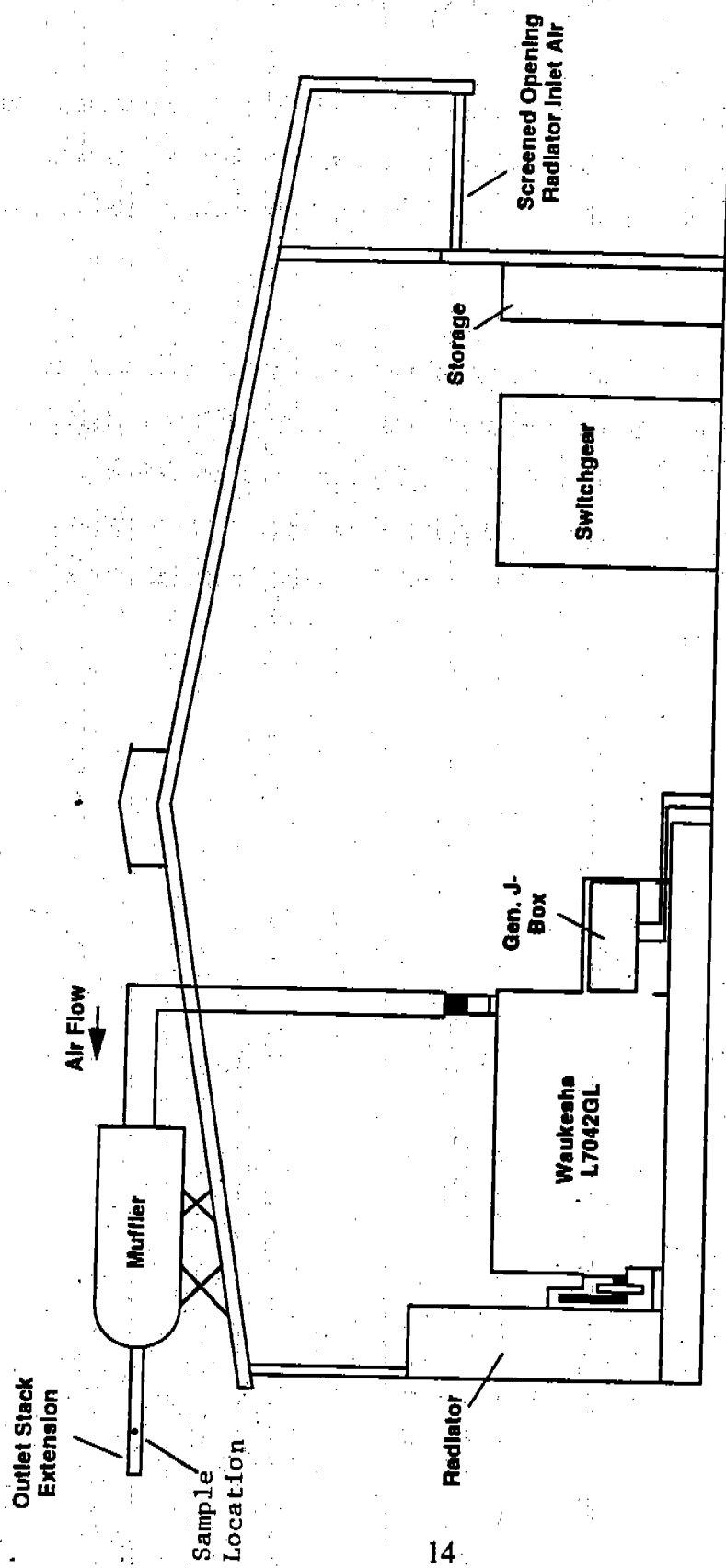


Figure 4-1. Stack Sampling Location.

SECTION 5

SAMPLING AND ANALYTICAL PROCEDURES

5.1 OVERVIEW

The compliance test program consisted of three test runs at the outlet location of the engine generator. Each test run was 60 minutes in length with a 30 minute moisture train per run. The test methods utilized, in accordance to 40 CFR Part 60 Appendix A, were as follows:

- Methods 1 and 2 Velocity Profile
- Method 3A O₂ and CO₂ Determination
- Method 4 Percent Moisture
- Method 9 Visible Emissions
- Method 6C SO₂ Determination
- Method 7E NO_x Determination
- Method 10 CO Determination
- Method 18 Methane Determination
- Method 25A Total Hydrocarbon Determination

5.2 PRESAMPLING ACTIVITIES

Presampling activities included: Equipment calibration; cleaning of the sample train glassware; and setup of the continuous emissions monitoring system for NO_x, CO, SO₂, THC, O₂, CO₂, and methane. The setup of the TCEMS and subsystems are described in detail in the following subsection.

5.2.1 Continuous Emission Monitoring

TRC followed procedures outlined in the EPA publication 340/1-83-016 regarding setup and operation of its transportable continuous emissions monitoring systems (TCEMS). The TCEMS

consists of three subsystems: sample acquisition/conditioning, sample analysis, and a data acquisition system (see Figure 5-1). The sample acquisition/conditioning unit is designed to deliver a representative sample of the stack gas stream to the sample analysis subsystem. Since the stream must be clean and dry for proper analyzer operation, a spun glass fiber filter, non-contact glass impinger train condenser, and a Permapure dryer were used for particulate and moisture removal. The sample line was heat traced to ensure that the flue gas maintained its vapor state as it was drawn to the monitors. Prior to the condensation removal system, a sample of the flue gas was analyzed for total hydrocarbons and methane.

Sample analyses were conducted using the following analyzers:

- a Horiba MFA 311A oxygen analyzer;
- a Siemens Ultramat 5E carbon monoxide analyzer;
- a Thermo Electron Model 10 oxide of nitrogen analyzer;
- a Horiba PIR2000 carbon dioxide analyzer;
- a Western Research sulfur dioxide analyzer;
- a Ratfisch total hydrocarbon analyzer;
- and a Hewlett Packard 5890 Series 2 FID/ECD gas chromatograph (GC).

In each case, accurate interpretation of analyzer response requires the systematic calibration of the instrument against gases of known concentrations. A calibration equation is determined from a linear regression of known gas concentrations versus instrument response. The equation used to convert instrument signal to concentration units follows:

$$\text{Concentration} = m * (\text{response}) + b$$

where:

m = slope of calibration curve

response = instrument signal (volts)

b = y - intercept of calibration curve

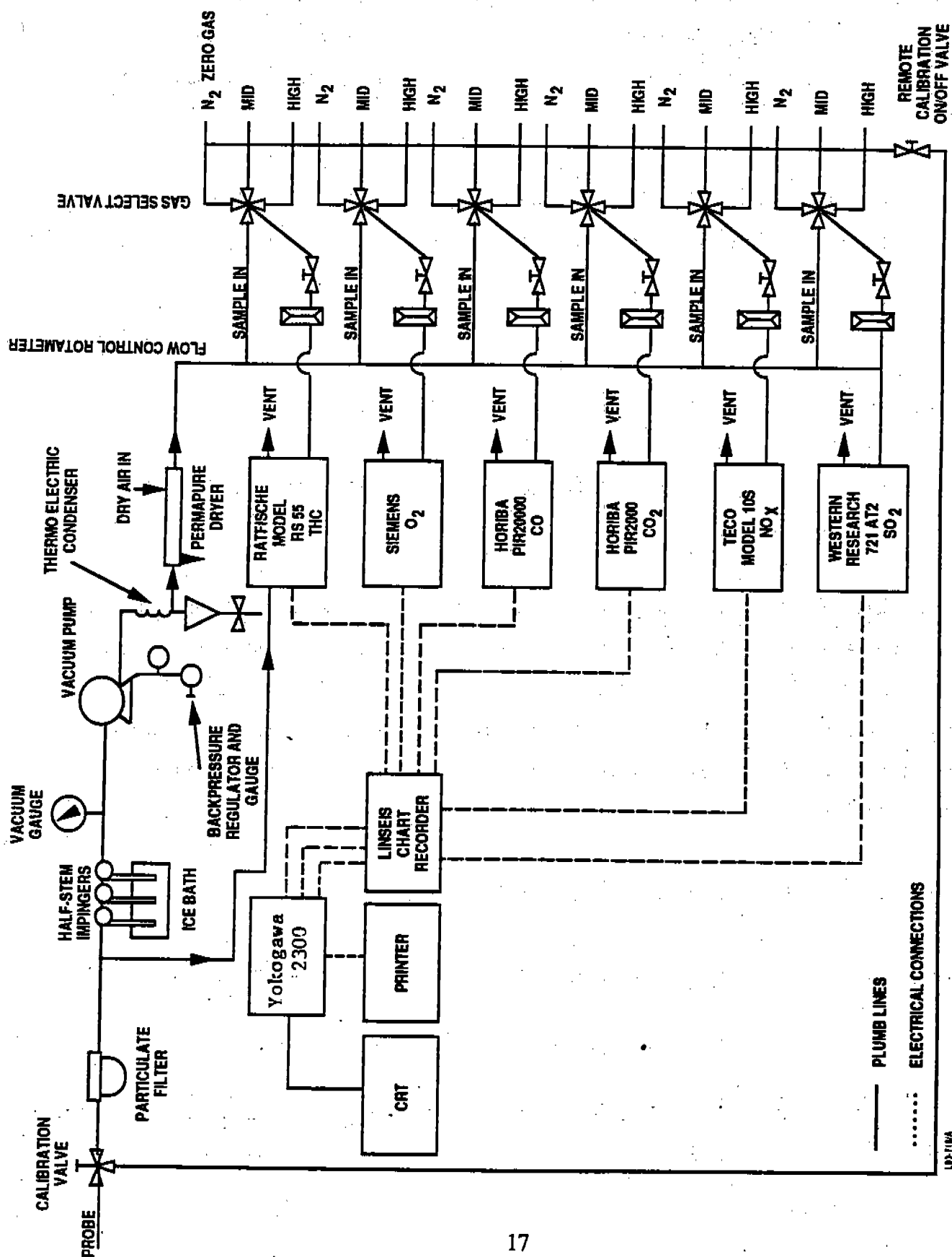


Figure 5-1. TCEM System Schematic.

The data acquisition subsystem consists of a Yokogawa data acquisition monitor which is designed to receive and log instrument signals (raw voltages) at user defined intervals. In addition, the Yokogawa was programmed to perform the previously mentioned concentration calculation.

Once the system was set up, the TCEMS was connected to a power source and brought on-line. Prior to sampling, the sample acquisition/conditioning system was leak checked by the following procedure:

- a. plug the system calibration line;
- b. observe that the flow of the rotameter's reaches zero Lpm;
- c. observe vacuum; and
- d. confirm that sample vacuum during sampling does not exceed vacuum attained during leak check.

The initial phase of instrumental analysis methods required calibration of all involved monitors. At the beginning of the day, direct instrument calibrations for zero and at minimum two upscale gases were performed prior to initiation of testing. Following the direct calibrations, system calibrations were performed both prior to and following each run using zero and one upscale gas concentration. These procedures allow for the determination of initial and final system bias, as well as system drift.

The calibration gas values and instrument range settings are listed below:

Gas	Calibration Gas Value	Instrument Range
NO _x	0, 122, 278, 505 ppm	0 - 1000 ppm
CO	0, 452, 957 ppm	0 - 1000 ppm
SO ₂	0, 21.1, 231, ppm	0 - 500 ppm

THC	0, 48.9, 102, 984 ppm	0 - 3000 ppm
CO ₂	0, 4.97, 10.1, 19.9 %	0 - 25 %
O ₂	0, 4.98, 10.1, 20.1 %	0 - 25 %

Calibration gases used are traceable to National Bureau of Standards Reference Materials. The measurement system performance specifications in 40 CFR 60 Appendix A Method 6C and 25A are listed below and were the performance criteria for this program.

Procedure	Performance Criteria (M6C)
Zero Calibration Error	< $\pm 2\%$ of the range
Calibration Error	< $\pm 2\%$ of the range
Zero Drift	< $\pm 3\%$ of the range
Calibration Drift	< $\pm 3\%$ of the range
Zero Bias	< $\pm 5\%$ of the range
Calibration Bias	< $\pm 5\%$ of the range
Response Time	≤ 30 seconds
Interference Response	< $\pm 2\%$ of the range
NO ₂ to NO Converter	> 90% conversion efficiency

Corrections to the measurement system or analyzer were made if the performance specifications were not met.

5.3 ONSITE SAMPLING ACTIVITIES

Onsite sampling activities included the determination of the response time of the CEM system, emission testing of the portable engine generator, and the collection of operational data.

5.3.1 Determination of the CEM System Response Time

After the CEM system was set up, response time was determined. Zero gas was introduced at the CEM system calibration gas valve assembly until a stable zero response was achieved. Once achieved, calibration gas was sent through the system with time allowed for a stable response. This procedure was conducted three times. A downscale response time was also conducted three times starting at a high span calibration value and switching to zero calibration gas. Time was allowed for a stable response. The performance specifications required that each measurement point be the sample time plus twice the response time.

5.3.2 Emission Testing for NO_x, CO, SO₂, THC, O₂, and CO₂

EPA Reference Methods 3A, 6C, 7E, 10, and 25A of 40 CFR 60 Appendix A were adhered to quantify emissions of O₂, CO₂, SO₂, NO_x, CO, and THC respectively. Emissions results are reported as ppm, lbs/hr and gm/HP-hr.

Prior to the testing of the engine, each analyzer was calibrated directly and through the system. Direct calibrations involved challenging the TCEMS with EPA Protocol 1 gas and setting the analyzers with zero and one upscale gas. The analyzer was then challenged with a second upscale gas. System calibration consisted of challenging the sampling system with zero gas and only one upscale gas. System calibration was conducted before and after each run with the final calibration the initial for the proceeding test run.

5.3.3 Emission Testing for Methane, Gas Chromatograph Analysis

Outlet flue gas samples were collected for methane utilizing EPA Method 18. An integrated flue gas sample was collected using a bag-in-drum technique. This procedure utilized a Tedlar bag placed inside a rigid container. The Tedlar bag was evacuated and attached to a 1/4 inch Teflon sample line which is attached to a stainless steel probe. Once the rigid container was placed under a slight vacuum equalization occurred and a sample of flue gas was drawn through the

sample line into the Tedlar bag. Sampling was conducted at an approximate rate of 0.35 Lpm for 60 minutes to yield a total sample volume of about 21 liters. These Tedlar bag samples were then analyzed by TRC's GC FID/ECD according to EPA Method 25C. Figure 5-2 presents a schematic of the Tedlar bag sampling system. GC data sheets are located in Appendix C. Total Gaseous Non-Methane Organic's (TGNMO) were determined using the difference between the THC ppm results and the methane ppm results. The following calculation was used:

$$\text{THC ppm} - \text{CH}_4 \text{ ppm} = \text{TGNMO ppm}$$

5.3.4 Visible Emission Observation

Method 9 of Appendix A Section 60 of the Federal Register and Section 3.12 of Volume III of the Quality Assurance Handbook were the basis of the visual observation procedures. Method 9 involves the determination of plume opacity by an EPA certified observer. Visible emissions observations were recorded on standard EPA-approved data forms following the procedures given in EPA Method 9. Readings were recorded every 15 seconds, in groups of four, for the duration of three 1-hour test runs. The field data sheets and the EPA certified observer's certificate can be found in Appendix D.

5.3.5 Velocity Measurements

Velocity measurements at the sampling location were made following EPA Reference Methods 1 and 2. A Type-S pitot tube with an attached inclined manometer was used to measure the exhaust velocities at the sampling location. An attached Type-K thermocouple with remote digital display was used to determine the flue gas temperature. During the test program, velocity measurements were made before and after each test. The required number of velocity measurements points for the sampling location was determined following EPA Method 1 for a nonparticulate gas stream.

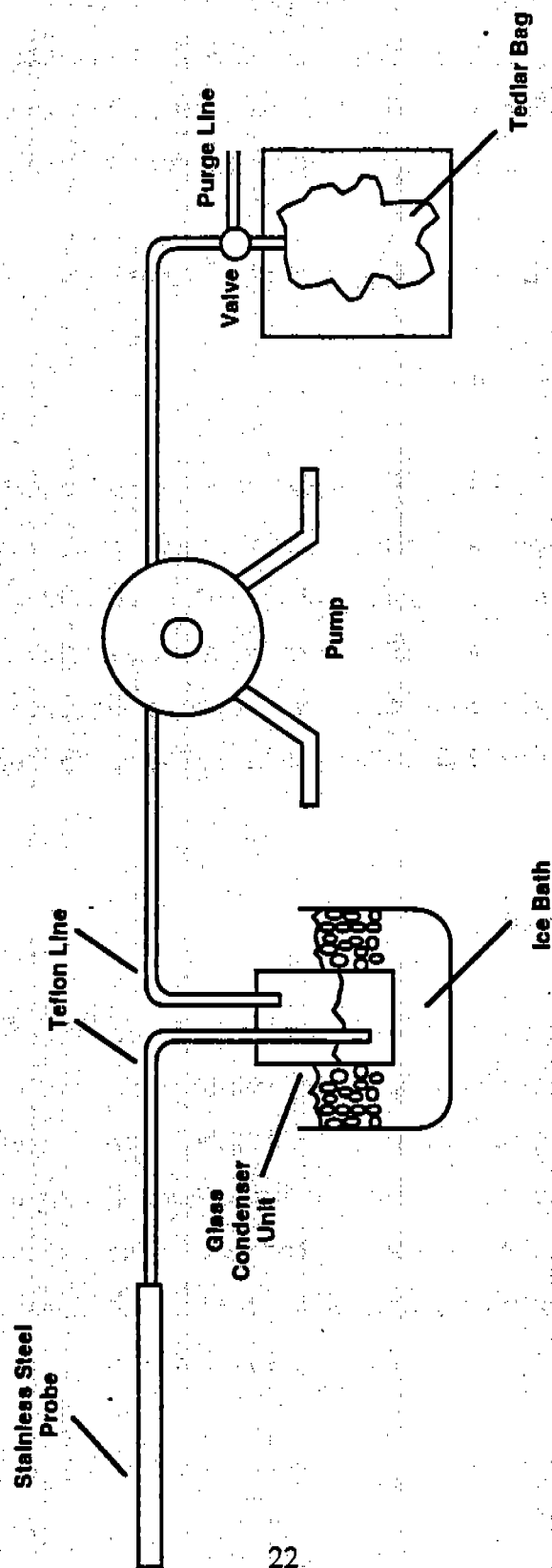


Figure 5-2. Tedlar Bag Sampling Schematic.

TRC

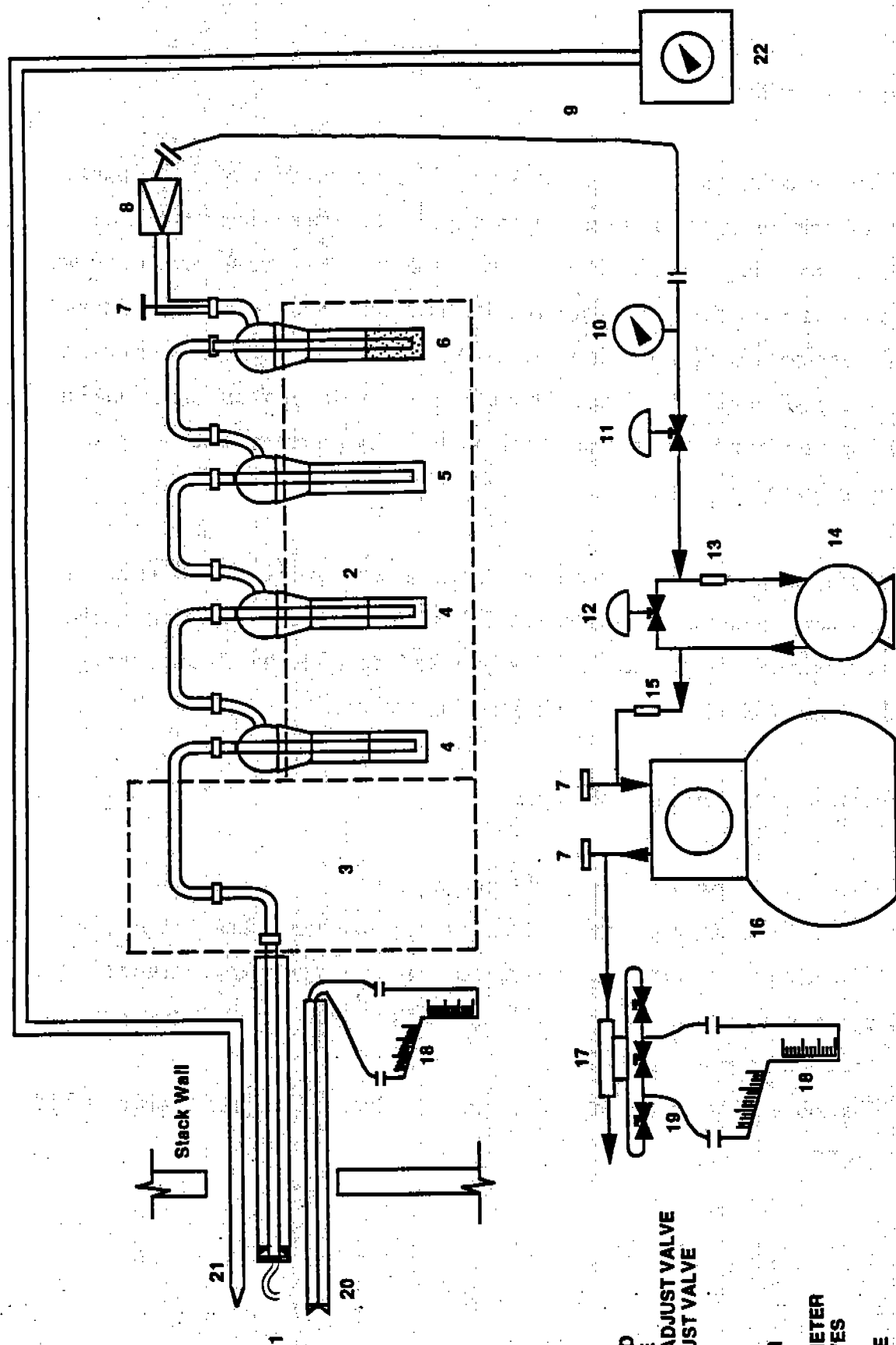
5.3.6 Moisture Determination

Moisture was determined for each test run according to EPA Reference Method 4. The moisture train was sampled from a single point positioned at the point of average velocity within the flue gas stream. A schematic diagram of the Method 4 train is given in Figure 5-3. Sample gas was drawn through a stainless steel probe into a series of four impingers designed for collection of moisture. The impinger system was as follows: 1st and 2nd - 100 ml deionized water; 3rd - empty; 4th - 200 g silica gel (for drying the gas stream and for moisture determination). Following the impinger system, the gas was drawn through a dry gas meter, a calibrated orifice and a leak-free oil fiber vane pump.

Leak checks on the train were performed before and after each sampling run. All leak checks and leakage rates were documented on the relevant field test data sheet. The acceptance criteria for the train is a maximum leakage rate of ≤ 0.02 cfm at the highest vacuum obtained during the run (post-test). The leak checks for every train passed this criteria.

Recovery procedures for the sampling train were:

1. Removed the sampling train to the recovery site.
2. Noted the condition of the train (i.e., impinger condition, silica gel color, etc.).
3. The contents of the first, second, and third impingers were measured in a precleaned graduated cylinder for moisture gain. Measurements were noted and the contents were discarded.
4. The silica gel was returned to its original container and weighed to obtain a final weight.



- 1). PROBE
- 2). ICE BATH
- 3). OVEN
- 4). 100 ml DI H₂O
- 5). EMPTY
- 6). SILICA GEL
- 7). THERMOMETER
- 8). CHECK VALVE
- 9). UMBILICAL CORD
- 10). VACUUM GAUGE
- 11). COARSE FLOW ADJUST VALVE
- 12). FINE FLOW ADJUST VALVE
- 13). OILER
- 14). VACUUM PUMP
- 15). FILTER
- 16). DRY GAS METER
- 17). ORIFICE TUBE
- 18). INCLINE MANOMETER
- 19). SOLENOID VALVES
- 20). PITOT
- 21). THERMOCOUPLE
- 22). PYROMETER

Figure 5-3. Method 4 Sampling Train Schematic.

SECTION 6

QUALITY ASSURANCE

6.1 OVERVIEW

TRC Environmental Corporation management is fully committed to an effective Quality Assurance/Quality Control Program whose objective is the delivery of a quality product. For much of TRC's work, that product is data resulting from field measurements, sampling, and analysis activities, engineering assessments, and the analysis of gathered data for planning purposes. The quality assurance program works to provide complete, precise, accurate, representative data in a timely manner for each project, considering both the project's needs and budget constraints. The company QA Director coordinates and directs the overall quality program with strong management support.

TRC's QA program conforms with EPA and NIOSH recommendations and is directed by the Company QA Director, a full-time professional who reports directly to the Company President. This give the QA Director the necessary authority and independence to find and correct any existing quality problems. A QA Scientist reports to the QA Director and assists in implementing the Company QA Program. Division QC Coordinators are responsible for the QC Program within each technical division; they report to both to their Division Manager and the Company QA Director.

This section highlights the specific QA/QC procedures followed on this test program. The responsible QA Officer for this program is the Company QA Scientist. He reviewed and approved the Protocol for this program and attended project review meetings to ensure that appropriate QA/QC procedures were being followed.

6.1.1 Calibration Procedures

Calibration of the field sampling equipment was performed prior to the field sampling effort.

Copies of the calibration sheets were submitted to the field team leader to take onsite and for the project file. Calibrations were performed as described in the EPA publication "Quality Assurance Handbook for Air Pollution Measurement Systems, Volume III, Stationary Source Specific Methods, EPA-600/4-77-027B". Equipment calibrated includes the sample metering system and pitot tubes. Calibration data sheets can be found in Appendix F.

6.1.2 Equipment Leak Checks

Prior to sampling, each sampling train was leak checked according to the procedures outlined in the applicable EPA Reference Method. Final leak checks were performed to ensure that no leaks developed in the train during the course of the test runs. Results of all leak checks performed can be found on the field data sheets presented in Appendix A.

6.1.3 Cyclonic Flow Check

The presence of cyclonic flow within the outlet stack was checked during the preliminary traverses. Cyclonic flow was not present in the outlet stack.

6.1.4 Calibration Gases

All calibration gases used to conduct instrument calibrations were prepared according to EPA Protocol 1, traceable to National Bureau of Standards Reference Materials.

6.1.5 Method 4 Sample Train

Prior to and at the conclusion of each run, the moisture train was leak checked to ensure that a representative moisture sample was obtained. All leak checks were completed successfully. Moisture gain was measured gravimetrically from the impingers and silica gel using an OHAUS triple beam balance accurate to 0.1 gram.

6.2 DATA REDUCTION AND VALIDATION

Extensive QC measures were used to ensure the generation of reliable data from sampling and analysis activities. Proper collection and organization of accurate information followed by clear and concise reporting of the data was a primary goal in this project.

6.2.1 Data Reduction

Data reduction performed in the field was limited to the following:

- EPA Method 4 Testing -- Check runs for sample volume, moisture, and associated parameters. These values were hand calculated on standardized forms (Appendix A) with an HP-11C Programmable Calculator and were also checked on a spreadsheet file with a portable computer.

Final data reduction included rechecking field calculations and logging all data into a calculating spreadsheet file via an AST PC.

6.2.2 Data Validation

The following criteria were used to evaluate data:

- use of approved test procedures;
- steady-state operation of the process being tested;
- use of properly operating and calibrated equipment;
- collection of the proper sample volumes as per the applicable methods.

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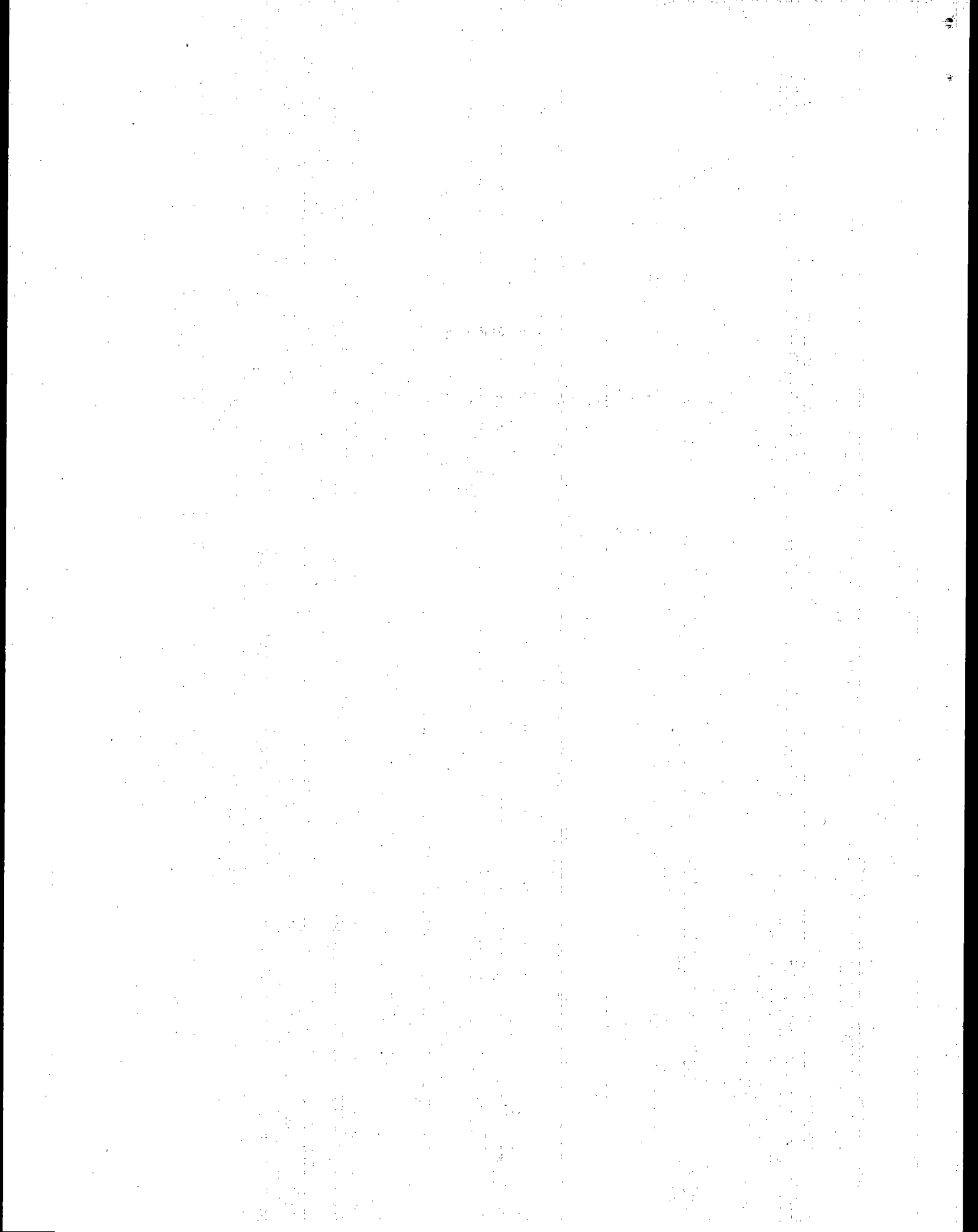
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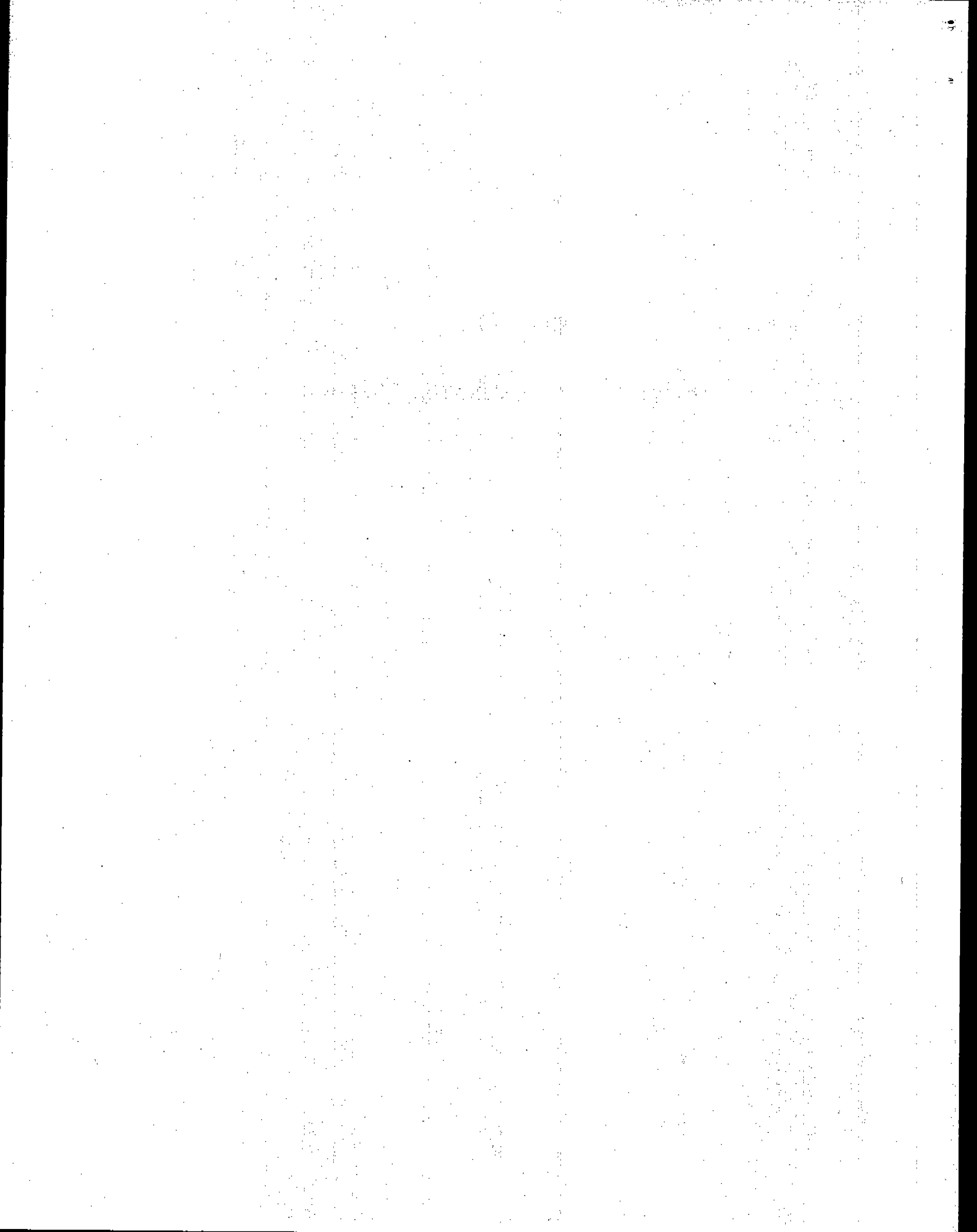
APPENDIX A

FIELD SAMPLING DATA SHEETS



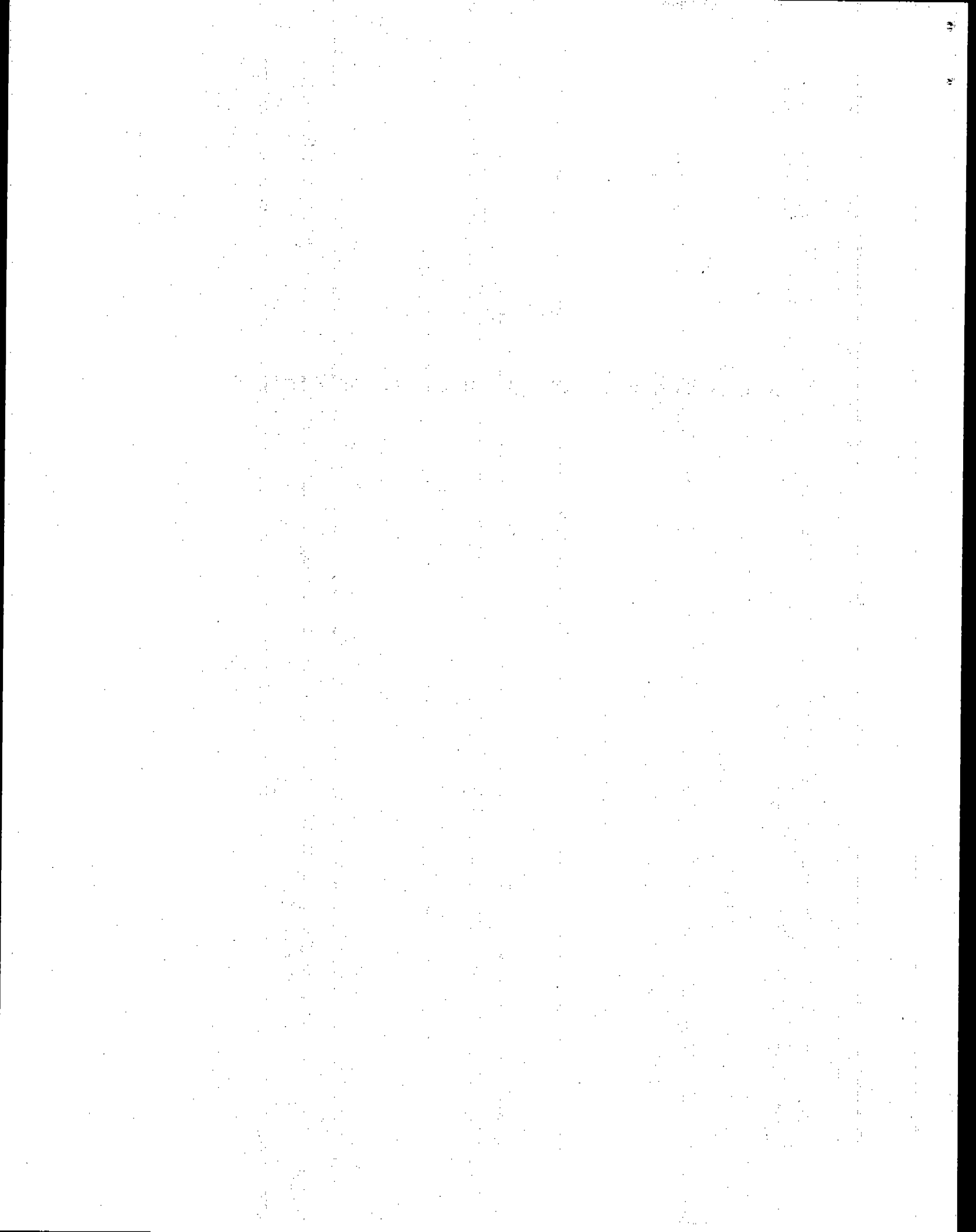
APPENDIX B

CEM DATA AND CALIBRATION SHEETS



APPENDIX C

GAS CHROMATOGRAPH DATA AND CALIBRATION SHEETS



APPENDIX D

V.E. OBSERVATION DATA AND CERTIFICATION SHEET

The first part of the document discusses the importance of maintaining accurate records of all transactions. It emphasizes that proper record-keeping is essential for the transparency and accountability of the organization. The document outlines the various methods used to collect and analyze data, ensuring that the information is reliable and valid.

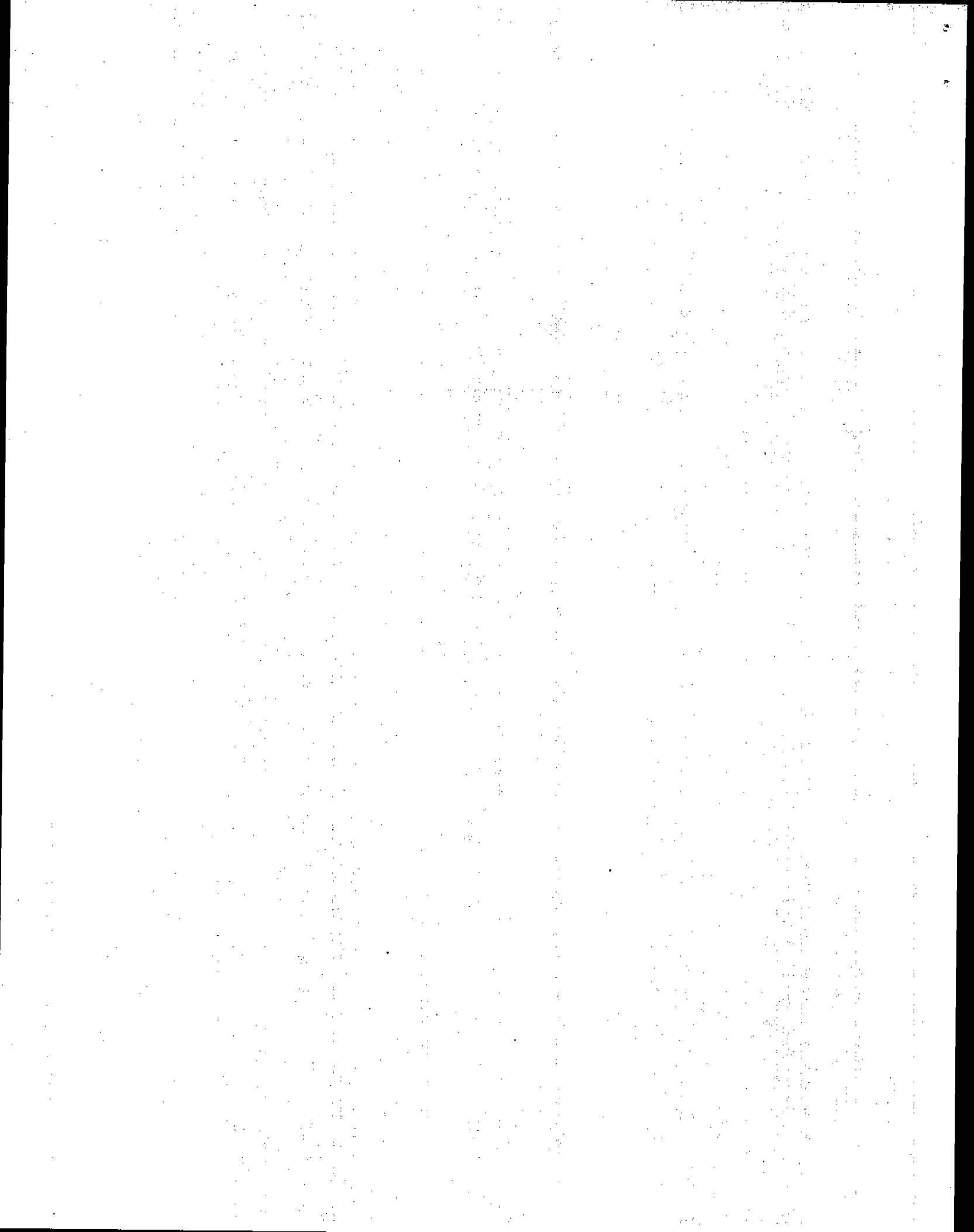
The second part of the document focuses on the implementation of the proposed system. It details the steps involved in the rollout, from initial testing to full-scale deployment. The document also addresses potential challenges and provides strategies to overcome them, ensuring a smooth transition to the new system.

The third part of the document discusses the ongoing monitoring and evaluation of the system. It highlights the need for continuous improvement and the importance of gathering feedback from users. The document provides a framework for assessing the system's performance and making necessary adjustments.

The final part of the document concludes with a summary of the key findings and recommendations. It reiterates the importance of the proposed system and encourages the organization to embrace the changes for long-term success.

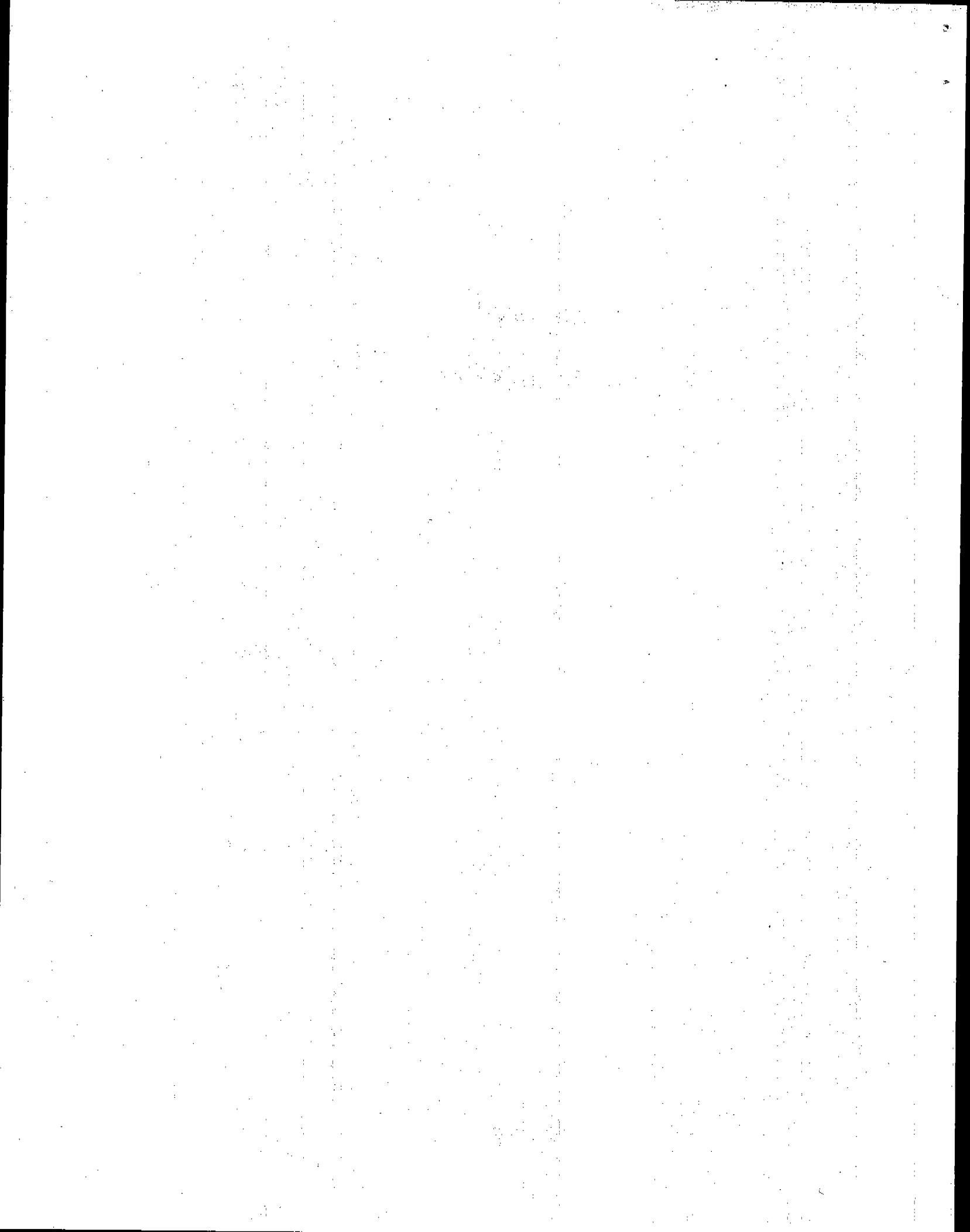
APPENDIX E

FACILITY PROCESS DATA



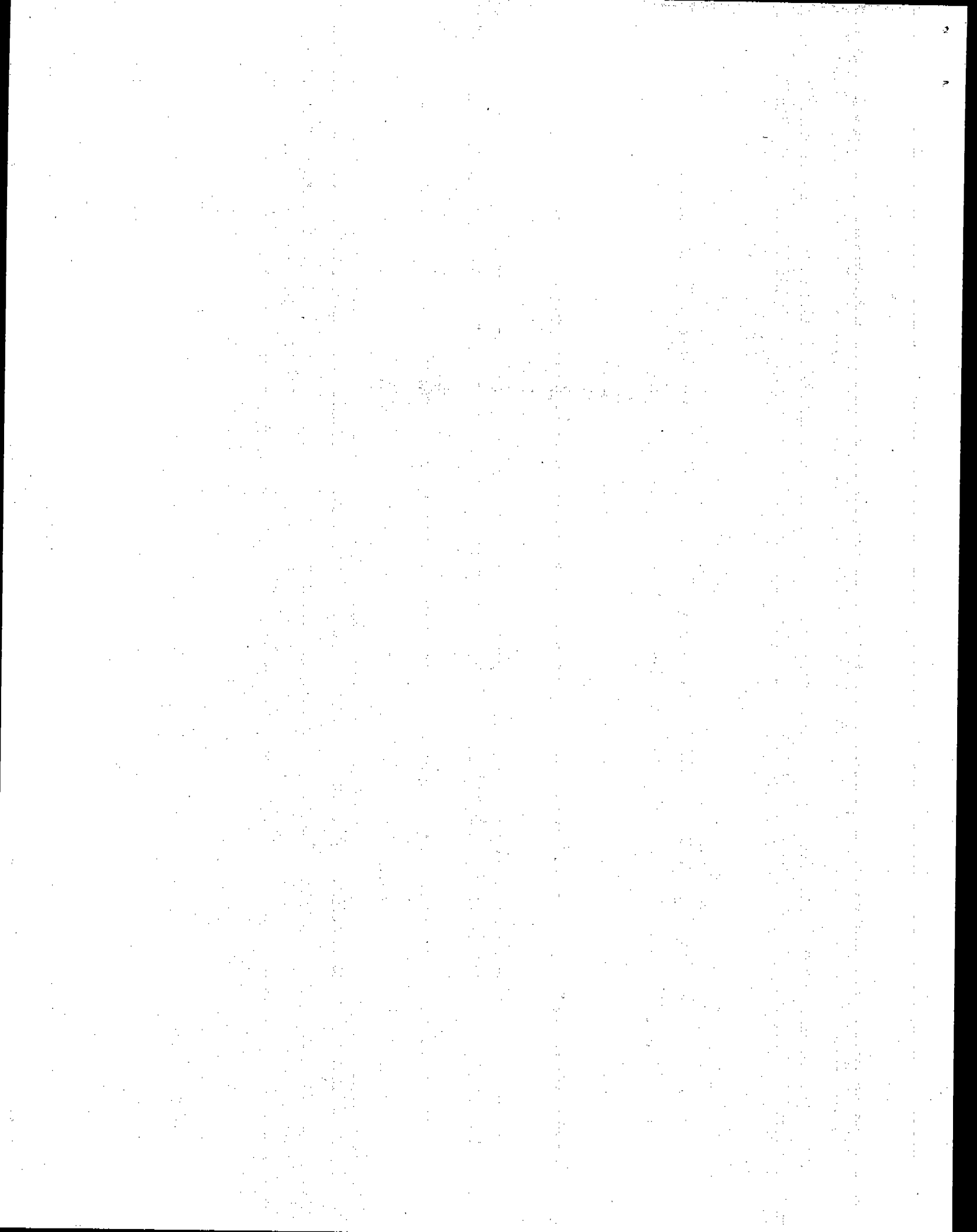
APPENDIX F

CALIBRATION SHEETS



APPENDIX A

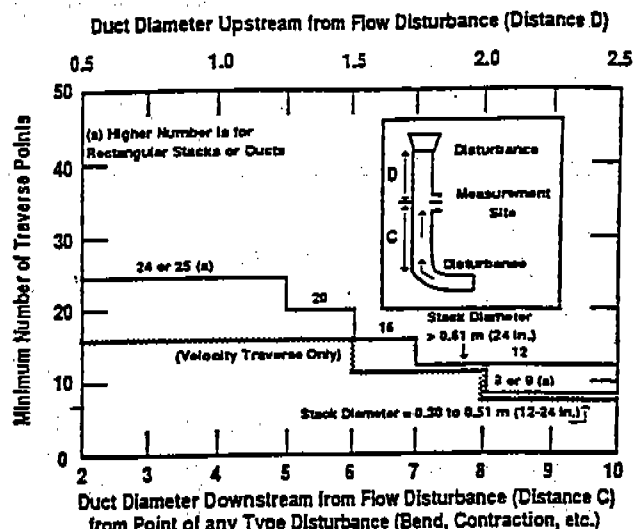
FIELD SAMPLING DATA SHEETS



Traverse Point Location for Circular and Rectangular Ducts

Project No.: _____
 Client: RF1 Chicopee
 Date: 12/13/93
 Sampling Location: outlet stack
 Internal Stack Diameter: 14"
 Nipple Length: 3 1/2"
 Total Stack Diameter: 17 1/2"
 Nearest Upstream Disturbance (C): _____
 Nearest Downstream Disturbance (D): _____
 Calculator: _____

Traverse Point Number	Fraction of Stack ID ($\frac{1}{100}$)	Stack ID	Traverse Point (1 + 2 = Point)	Nipple Length	Traverse Point Inside of Far Wall to Outside of Port Nipple (3 + 4 = Point)
1	.032	14	.448	3.5	3.95
2	.105	14	1.47	4.97	4.97
3	.194	14	2.716	6.22	6.22
4	.323	14	4.522		8.02
5	.677	14	9.478		12.77
6	.806	14	11.28		14.78
7	.895	14	12.53		16.03
8	.965	14	13.55		17.05
9					
10					
11					
12					
13					
14					
15					
16					
17					
18					
19					
20					
21					
22					
23					
24					



$$\text{Rectangular Duct Equivalent Diameter Determination} = \frac{2xLxW}{L+W}$$

Location of Traverse Points in Circular Stacks

	4	6	8	10	12	14	16	18	20	22	24
1	5.7	4.4	3.2	2.6	2.1	1.3	1.6	1.4	1.3	1.1	1.1
2	25.0	14.6	10.5	8.2	6.7	5.7	4.9	4.4	3.9	3.5	3.2
3	75.0	29.6	19.4	14.6	11.8	9.9	8.5	7.5	6.7	6.0	5.5
4	93.3	70.4	32.3	22.6	17.7	14.6	12.5	10.9	9.7	8.7	7.9
5		85.4	67.7	34.2	25.0	20.1	16.9	14.6	12.9	11.6	10.5
6		95.6	80.6	65.8	35.6	26.9	22.0	18.8	16.3	14.6	13.2
7			89.5	77.4	64.4	36.6	28.3	23.6	20.4	18.0	16.1
8			96.8	85.4	75.0	63.4	37.5	29.6	25.0	21.8	19.4
9				91.8	82.3	73.1	62.5	38.2	30.6	26.2	23.0
10				97.4	88.2	79.9	71.7	61.8	38.8	31.5	27.2
11					93.3	85.4	78.0	70.4	61.2	39.3	32.3
12					97.9	90.1	83.1	76.4	69.4	60.7	39.8
13						94.3	87.5	81.2	75.0	68.5	60.2
14						98.2	91.5	85.4	79.6	73.8	67.7
15							95.1	89.1	83.5	78.2	72.8
16							98.4	92.5	87.1	82.0	77.0
17								95.6	90.3	85.4	80.6
18								98.6	93.3	88.4	83.9
19									96.1	91.3	86.8
20									98.7	94.0	89.5
21										96.5	92.1
22										98.9	94.5
23											96.8
24											98.9

Location of Traverse Points in Rectangular Stacks

	2	3	4	5	6	7	8	9	10	11	12
1	25.0	16.7	12.5	10.0	8.3	7.1	6.3	5.6	5.0	4.5	4.2
2	75.0	50.0	37.5	30.0	25.0	21.4	18.8	15.7	13.0	13.6	12.5
3		83.3	62.5	50.0	41.7	35.7	31.3	27.8	25.0	22.7	20.8
4			87.5	70.0	58.3	50.0	43.8	38.9	35.0	31.8	29.2
5				90.0	75.0	64.3	56.3	50.0	45.0	40.9	37.5
6					91.7	78.6	68.8	61.1	55.0	50.0	45.8
7						92.9	81.3	72.2	65.0	59.1	54.2
8							93.8	83.3	75.0	68.2	62.5
9								94.4	85.0	77.3	70.8
10									95.0	85.4	79.2
11										95.5	87.5
12											95.8

Field Moisture Determination

Client: BFI

Project No.: _____

Location: Chicopee

Date: 12/14/93

Run No.: 1

Operator: B. H. Kissel

Data

PM

Min	Clock Time min sec	Gas Meter C.F. VM	TM In	TM Out	Orifice In. H ₂ O (+)	Vac. Gage In. Hg (-)	Imp temp
0	0:00	236.124	92	92	2.0	9.25	75
5	4:59	238.890	93	93	2.0	9.50	71
10	9:59	243.560	95	93	2.0	9.50	73
15	15:01	247.260	97	93	2.0	9.50	75
20	19:57	250.890	99	94	2.0	9.50	77
25	25:16	254.760	101	94	2.0	9.50	79
30	30:00	258.239	103	95	2.0	9.50	80
Total/Avg							

Impingers

	1	2	3
Final mL	<u>147</u>	<u>100</u>	<u>0</u>
Initial mL	<u>100 mL</u>	<u>100 mL</u>	<u>0</u>
Net mL	<u>47</u>	<u>0</u>	<u>0</u>
Total moisture (Net mL + Net gm) = _____			

Silica Gel

Container No. _____
 Final gm 331.40
 Initial gm 326.80
 Net gm _____

Calculations

- (1) PB = 29.39 Meterbox No. 8130
- (2) VM Net = _____ Y = DGM Calibration Factor = .98 DHE 1.68
- (3) TM Avg = _____ TM + 460 _____
- (4) PM Avg = + _____ Orifice In. H₂O x $\frac{1}{13.6}$ = + _____ orifice In. Hg.
 = _____ Vacuum gage In. Hg (when meter is before pump)
- (5) VMSTD = $\frac{528 \times \text{VM} (\text{PB} + \text{PM}) (\text{Y})}{29.92 \times (\text{TM} + 460)}$ = _____
- (6) VW = mL H₂O + gm Silica gel = _____
- (7) VW Gas = VW x 0.04715 = _____
- (8) %M = $\frac{100 \times \text{VW Gas}}{\text{VMSTD} + \text{VW Gas}}$ = $\frac{100 \times (\quad)}{(\quad) + (\quad)}$ = $\frac{(\quad)}{(\quad)}$ = _____

1000 1000 1000 1000 1000 1000 1000 1000 1000 1000

Field Moisture Determination

Client: BFI

Project No.: _____

Location: Chicopee

Date: 12/14

Run No.: 2

Operator: B. H. Kussel

Data

PM

Min	Clock Time	Gas Meter C.F. VM	TM In	TM Out	Orifice In. H ₂ O (+)	Vac. Gage In. Hg (-)	Imp Temp
0	0:00	259.913	95	95	2.0	5.0	76
5	5:07	263.630	100	96	1.9	5.0	75
10	10:10	267.420	103	96	2.0	5.5	75
15	15:03	271.080	105	97	2.0	5.5	78
20	20:04	274.830	105	97	2.0	5.5	79
25	25:03	278.560	106	97	2.0	5.5	81
30	30:00	282.274	107	97	2.0	5.5	82
Total/Avg							

Impingers

Silica Gel

	1	2	3
Final mL	<u>148</u>	<u>100</u>	<u>0</u>
Initial mL	<u>100</u>	<u>100</u>	<u>0</u>
Net mL	_____	_____	_____
Total moisture (Net mL + Net gm) =	_____		

Container No. _____

Final gm 351.00g

Initial gm 344.60g

Net gm _____

Calculations

- (1) PB = 29.39 Meterbox No. 8130
- (2) VM Net = _____ Y = DGM Calibration Factor = .98 ΔH₂O 1.88
- (3) TM Avg = _____ TM + 460 _____
- (4) PM Avg = + _____ Orifice In. H₂O x $\frac{1}{13.6}$ = + _____ orifice In. Hg.
= - _____ Vacuum gage In. Hg (when meter is before pump)
- (5) VMSTD = $\frac{528 \times \text{VM} (\text{PB} + \text{PM}) (\text{Y})}{29.92 \times (\text{TM} + 460)}$ = _____
- (6) VW = mL H₂O + gm Silica gel = _____
- (7) VW Gas = VW x 0.04715 = _____
- (8) %M = $\frac{100 \times \text{VW Gas}}{\text{VMSTD} + \text{VW Gas}}$ = $\frac{100 \times ()}{() + ()}$ = $\frac{()}{()}$ = _____

Leak check initial @ 10 mm Hg .011
@ 7 mm Hg .005

Field Moisture Determination

Client: BFI

Project No.: _____

Location: Chicopee

Date: 12/14/93

Run No.: 3

Operator: B. Kissel

Data

PM

Min	Clock Time	Gas Meter C.F. VM	TM In	TM Out	Orifice In. H ₂ O (+)	Vac. Gage In. Hg (-)	Imp temp
0	0:00	282.679	96	95	2.0	7.0	73
5	4:55	286.370	97	97	2.0	6.75	73
10	9:55	290.120	103	97	2.0	6.75	72
15	14:54	293.810	105	97	2.0	6.75	72
20	20:20	297.920	106	97	2.0	6.75	72
25	25:07	301.510	106	97	2.0	6.75	BT
30	30:00	305.207	105	97	2.0	6.75	81
Total/Avg							81

Impingers

	1	2	3
Final mL	<u>149</u>	<u>100</u>	<u>0</u>
Initial mL	<u>100</u>	<u>100</u>	<u>0</u>
Net mL	<u>49</u>	<u>0</u>	<u>0</u>
Total moisture (Net mL + Net gm) =	<u>57.49</u>		

Silica Gel

Container No. _____
 Final gm 328.50
 Initial gm 320.01
 Net gm 8.49

Calculations

- (1) PB = 29.39
 Meterbox No. _____
 (2) VM Net = _____
 Y = DGM Calibration Factor = _____
 (3) TM Avg = _____
 TM + 460 _____
 (4) PM Avg = + _____ Orifice In. H₂O x 13.6 = + _____ orifice In. Hg.
 = - _____ Vacuum gage In. Hg (when meter is before pump)
 (5) VMSTD = $\frac{528 \times VM - (PB + PM) (Y)}{29.92 \times (TM + 460)}$ = _____
 (6) VW = mL H₂O + gm Silica gel = _____
 (7) VW Gas = VW x 0.04715 = _____
 (8) %M = $\frac{100 \times VW \text{ Gas}}{VMSTD + VW \text{ Gas}}$ = $\frac{100 \times ()}{() + ()}$ = $\frac{()}{()}$ = _____

back check @ 10 mH₂O

Stack Geometry & Gas Velocity Data

Page of

Project No.

Source

Client BFI

Sample Location Outlet Stack

Plant Chicopee

Run No. 1

Operator B. Knell

Static, In. H₂O

Meter Box No. 8130

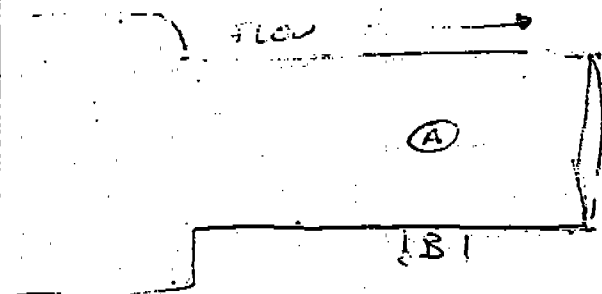
Sketch of Sampling Location

Time (24 hr. Clock)	Sample Point	Stack Temp. °F or °C	Manom. Reading In. H ₂ O	Cyclonic Flow Null Angle
1131	1A	706	2.0	
	2A	709	2.1	
	3A	713	2.3	
	4A	718	2.3	
	5A	721	2.4	
	6A	720	2.3	
	7A	717	2.4	
1132	8A	680	2.2	
134	1B	704	2.4	
	2B	708	2.1	
	3B	712	2.3	
	4B	716	2.3	
	5B	719	2.3	
	6B	720	2.4	
	7B	717	2.4	
1136	8B	715	2.4	

Stack Diameter

Diameters Upstream

Diameters Downstream



Wet Bulb

Dry Bulb

%M

TRC

• 研究

•

Source _____

Sample Location Outlet Stack

Run No. Final Run / Initial 2

Static, ln. H₂O 1.5

Sketch of Sampling Location

Stack Diameter 14"

Diameters Upstream _____

Diameters Downstream _____



Дру Вулф

%M _____

Stack Geometry & Gas Velocity Data

Page of

Project No.

Source

Client BFI

Sample Location Outlet Stack

Plant Chicago

Run No. Final run 2 Initial run 3

Operator Bill Lamb

Static, In. H₂O 2.50

Meter Box No. 8130

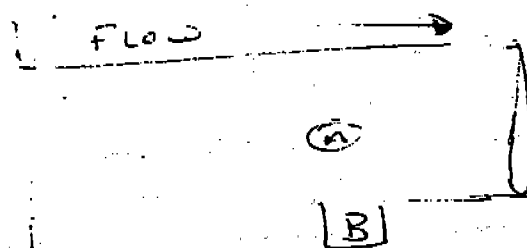
Sketch of Sampling Location

Time (24 hr. Clock)	Sample Point	Stack Temp. °F or C°	Manom. Reading In. H ₂ O	Cyclonic Flow Null Angle
1500	1A	704	2.20	
	2A	711	2.30	
	3A	717	2.30	
	4A	720	2.40	
	5A	720	2.40	
	6A	719	2.50	
	7A	716	2.50	
1503	8A	706	2.40	
1505	1B	690	1.80	
	2B	705	2.20	
	3B	714	2.30	
	4B	718	2.50	
	5B	720	2.60	
	6B	721	2.60	
	7B	717	2.60	
1508	8B	713	2.50	

Stack Diameter

Diameters Upstream

Diameters Downstream



Wet Bulb

Dry Bulb

%M

Project No. Client BFIPlant CherokeeOperator Bill KinsMeter Box No. 8130Source Sample Location Outlet StackRun No. 3 Final RunStatic, In. H₂O 2.0

Time (24 hr. Clock)	Sample Point	Stack Temp. °F or °C	Manom. Reading In. H ₂ O	Cyclonic Flow Null Angle
1637	1A	674	2.0	
	2A	698	2.2	
	3A	704	2.4	
	4A	708	2.5	
	5A	712	2.5	
	6A	713	2.6	
	7A	712	2.6	
1639	8A	708	2.5	
1641	1A	660	1.6	
	2A	693	2.2	
	3A	704	2.5	
	4A	709	2.5	
	5A	714	2.5	
	6A	716	2.6	
	7A	715	2.5	
1642	8A	707	2.4	

Sketch of Sampling Location

Stack Diameter Diameters Upstream Diameters Downstream Wet Bulb Dry Bulb %M

BFI CHICOPEE

STACK #1

14 December 1993

	Run #1		Run #2		Run #3	
	Area Counts	Concentration (PPM)	Area Counts	Concentration (PPM)	Area Counts	Concentration (PPM)
Injection #1	1181868	2020.9	1212805	2074.2	1165685	1993.0
Injection #2	1193205	2040.4	1199243	2050.8	1173062	2005.7
Injection #3	1212390	2073.5	1192089	2038.5	1161044	1985.0
Average	1195821	2044.9	1201979	2054.5	1166597	1994.6

DRAFT

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of pages > 1

To: Mike O'Brien	From: Tim Senger
Co: TRC / CO BFI	Co: TRC
Dept: Air	Phone: X5158
Fax: 413 592 8169	Fax: 508 453 1995

APPENDIX B

CEM DATA AND CALIBRATION SHEETS

FACILITY: BFI CHICOPEE LANDFILL
SOURCE: DIESEL ENGINE GENERATOR
MONTH/YR: DECEMBER 14, 1993

CEM DATA CORRECTION PROGRAM
INSTRUMENTAL REFERENCE METHODS - 3A, 7E, 10,

	O ₂ %	CO ₂ %	NO _x ppm	SO ₂ ppm	THC, ppm	CO, ppm
RUN 1 12/14/93	25 0	25 0	1000 0	500 0	3000 0	1000 0
SLOPE/Y-INT	0	0	0	0	0	0
SYS CAL VALUES ZERO/SPAN	10.1	10.1	505	505	231	452.2
DIR CAL ZERO VDC/CONC	0.04	0.03	1	1	0	1
DIR CAL SPAN VDC/CONC	10.01	10.08	505	505	235	448
INT SYS ZERO VDC/CONC	0.00	0.04	11	11	0	1
FIN SYS ZERO VDC/CONC	0.00	0.03	15	15	3	2
INT SYS SPAN VDC/CONC	9.95	10.02	504	504	207	445
FIN SYS SPAN VDC/CONC	9.88	9.95	506	506	215	445
INT/FIN SYS BIAS ZERO %	-0.16	0.04	1.00	0.00	0.00	0.00
INT/FIN SYS BIAS SPAN %	-0.52	-0.24	-0.10	-5.60	-0.17	0.10
ZERO/SPAN SYS DRIFT %	-0.28	-0.04	0.40	0.20	0.00	-0.30
ANALYZER SCALE(SPAN)	25	25	1000	500	3000	1000
RUN AVG	8.78	10.87	89.00	1.00	2127.00	495.00
CORR. AVG	8.94	11.00	78.01	-0.55	2120.53	447.84

	O ₂ %	CO ₂ %	NO _x ppm	SO ₂ ppm	THC, ppm	CO, ppm
RUN 2 12/14/93	25 0	25 0	1000 0	500 0	3000 0	1000 0
SLOPE/Y-INT	0	0	0	0	0	0
SYS CAL VALUES ZERO/SPAN	10.1	10.1	505	505	231	452.2
DIR CAL ZERO VDC/CONC	0.04	0.03	1	1	0	1
DIR CAL SPAN VDC/CONC	10.01	10.08	505	505	235	448
INT SYS ZERO VDC/CONC	0.00	0.03	15	15	3	2
FIN SYS ZERO VDC/CONC	-0.04	0.03	19	19	2	1
INT SYS SPAN VDC/CONC	9.88	9.95	506	506	215	445
FIN SYS SPAN VDC/CONC	9.41	9.83	519	519	214	445
INT/FIN SYS BIAS ZERO %	-0.32	0.00	1.40	0.60	0.00	0.00
INT/FIN SYS BIAS SPAN %	-2.40	-0.52	0.10	-4.00	0.10	-0.30
ZERO/SPAN SYS DRIFT %	-1.88	0.00	0.40	-0.20	0.13	-0.10
ANALYZER SCALE(SPAN)	25	25	1000	500	3000	1000
RUN AVG	8.75	10.85	90.00	2.00	2157.00	494.00
CORR. AVG	9.16	11.08	74.40	-0.54	2146.28	447.01

	O ₂ %	CO ₂ %	NO _x ppm	SO ₂ ppm	THC, ppm	CO, ppm
RUN 3 12/14/93	25 0	25 0	1000 0	500 0	3000 0	1000 0
SLOPE/Y-INT	0	0	0	0	0	0
SYS CAL VALUES ZERO/SPAN	10.1	10.1	505	505	231	452.2
DIR CAL ZERO VDC/CONC	0.04	0.03	1	1	0	1
DIR CAL SPAN VDC/CONC	10.01	10.08	505	505	235	448
INT SYS ZERO VDC/CONC	-0.04	0.03	19	19	2	1
FIN SYS ZERO VDC/CONC	-0.04	0.03	16	16	2	1
INT SYS SPAN VDC/CONC	9.41	9.83	519	519	214	444
FIN SYS SPAN VDC/CONC	9.84	9.92	519	519	218	444
INT/FIN SYS BIAS ZERO %	-0.32	0.00	1.80	0.40	0.13	0.00
INT/FIN SYS BIAS SPAN %	-2.40	-1.00	1.40	-4.20	0.03	-0.40
ZERO/SPAN SYS DRIFT %	1.72	0.36	-0.30	0.00	-0.10	0.00
ANALYZER SCALE(SPAN)	25	25	1000	500	3000	1000
RUN AVG	8.89	10.72	83.00	3.00	2163.00	482.00
CORR. AVG	9.33	10.97	65.96	1.08	2156.12	437.14

ANALYZER DAILY CALIBRATION CHECK

Location BFL Chicago
 Date 12/14/93
 Day _____

TIME START/STOP 0940
 PERFORMED BY WCB/ra

Contract _____

INSTRUMENT RESPONSE Direct Cal

Instrument	Zero		1		2		3		4	
	Conc.	Response	Conc.	Response	Conc.	Response	Conc.	Response	Conc.	Response
O ₂ 0-25	0	0.04	4.98	4.95	10.1	10.01	20.1	19.97		
CO ₂ 0-25	0	8.103	4.97	4.78	10.1	10.08	19.9	19.49		
CO 0-100	0	1.0			482.2	448	95.7	94.7		
SO ₂ 0-500	0	0.0	21.1	20.0	251	235	251			
NH ₃ 0-1000	0	1	122	130	278	287	505	505		
TIC 0-3000	0	0	48.9	47	102	95	9840	988		
TIC										

CALIBRATION EQUATION

$$y = mx + b$$

O₂ _____
 CO₂ _____
 SO₂ _____
 NO_x _____
 HCl _____
 m _____
 b _____
 corr. ² _____
 coeff r _____

ANALYZER DAILY CALIBRATION CHECK

Contract _____

Location BF/Chicago

TIME START/STOP _____

Date 12/14/93

PERFORMED BY MO'Brien

Day _____

Initial Run 1 Eng 1

INSTRUMENT RESPONSE Initial System Cal

Final Run 1

Instrument	Zero		1		2		3		4	
	Conc.	Response	Conc.	Response	Conc.	Response	Conc.	Response	Conc.	Response
O ₂	0	0.00	10.1	9.95			0	0.00	10.1	9.88
CO ₂	0	1.04	10.1	10.02			0	0.03	10.1	9.95
CO	0	1	452.2	445			0	2.0	452.2	445
SO ₂	0	0.0	231	207			0	3	231	215
NO _x	0	11	505	504			0	15	505	506
THC	0	0	984	983			0	0	984	991
THC										

CALIBRATION EQUATION

$$y = mx + b$$

O₂

CO₂

CO

SO₂

NO_x

HC1

m

b

corr. r²
coeff r

ANALYZER DAILY CALIBRATION CHECK

Location BFI Chicago WA

TIME START/STOP _____

Contract _____

Date 12/14/93

PERFORMED BY MD'Brien

Day _____

Final Run 2

Final Run 3

INSTRUMENT RESPONSE

Instrument	Zero		1		2		3		4	
	Conc.	Response	Conc.	Response	Conc.	Response	Conc.	Response	Conc.	Response
O ₂	0	-0.04	10.1	9.41			0	0.04	10.1	9.84
CO ₂	0	0.03	10.1	9.83			0	0.03	10.1	9.92
CO	0	1.0	45.20	44.4			0	1.0	45.20	44.4
SO ₂	0	5.0	231	214			0	2.0	231	218
H ₂ X	0	1.9	505	519			0	16.0	505	519
THC	0	4.0	984	989			0	1.0	984	988
THC										

CALIBRATION EQUATION

$$y = mx + b$$

O₂

CO₂

CO

SO₂

NO_x

HCl

m

b

corr. %
coeff r²

616-900

TRC

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FBI - MEMPHIS

ENCLOSURE
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CHY-1

17 JUL 1992

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02 26th
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2. **Curriculum**

27/11/93
JVC
88

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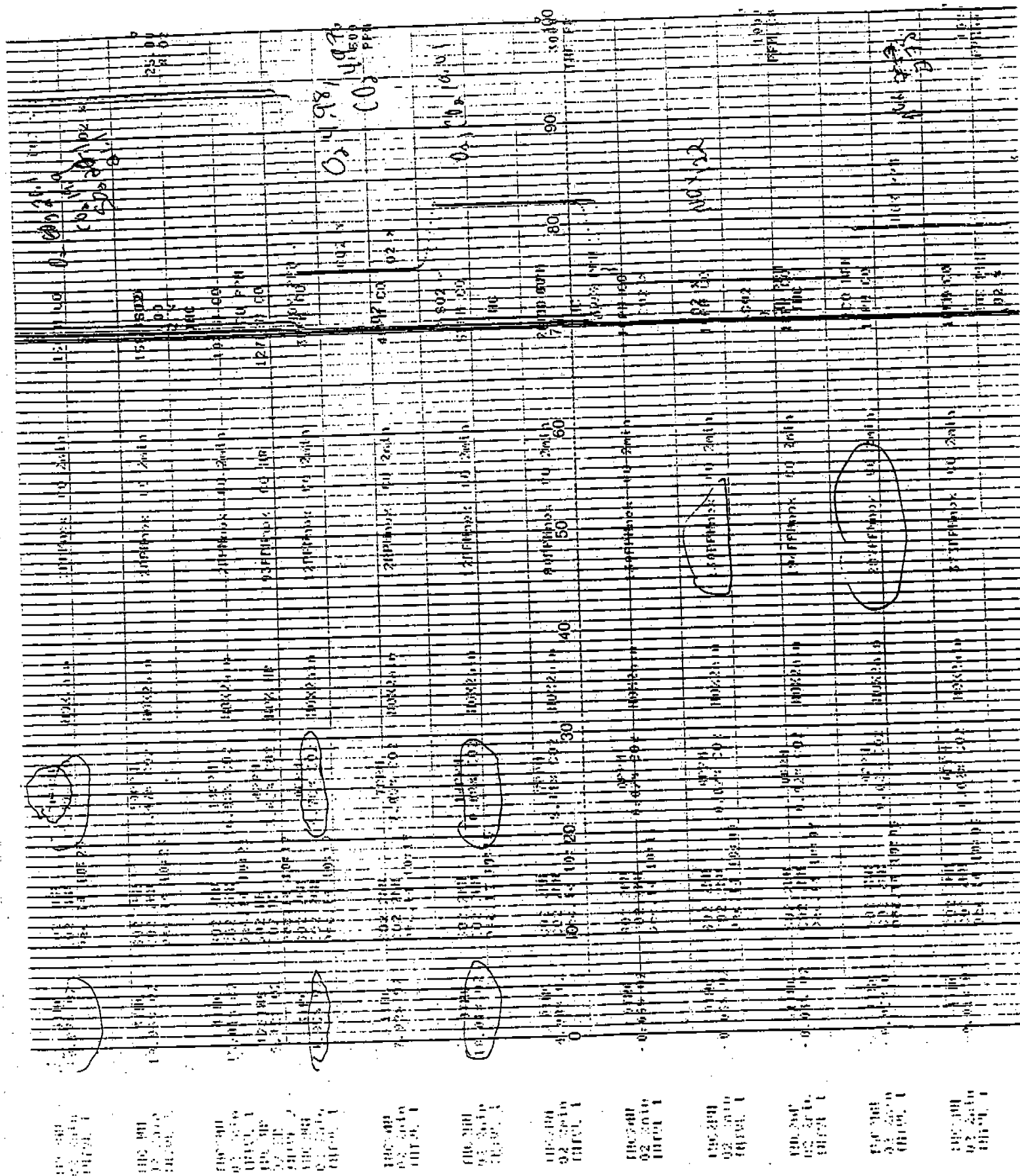
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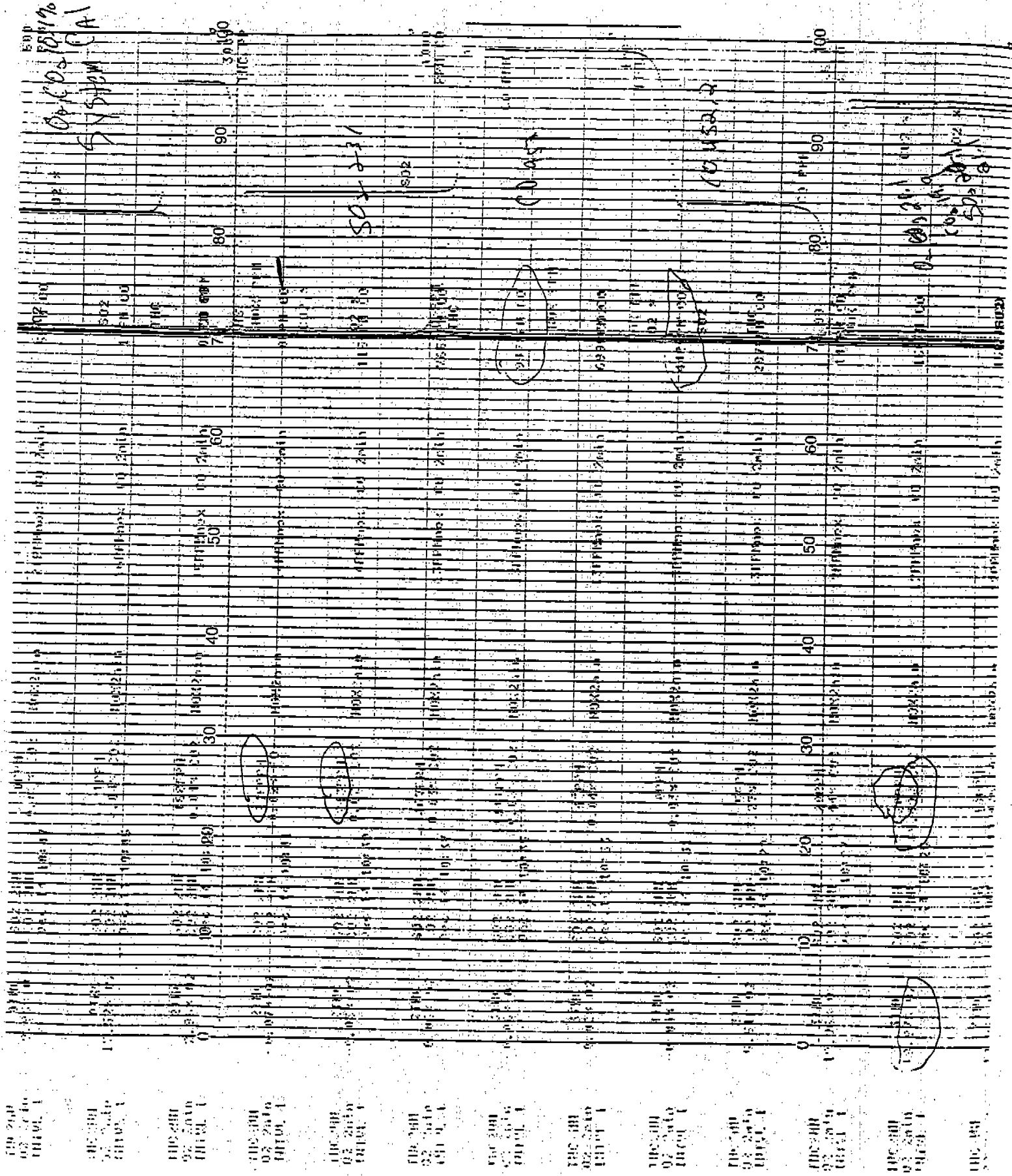
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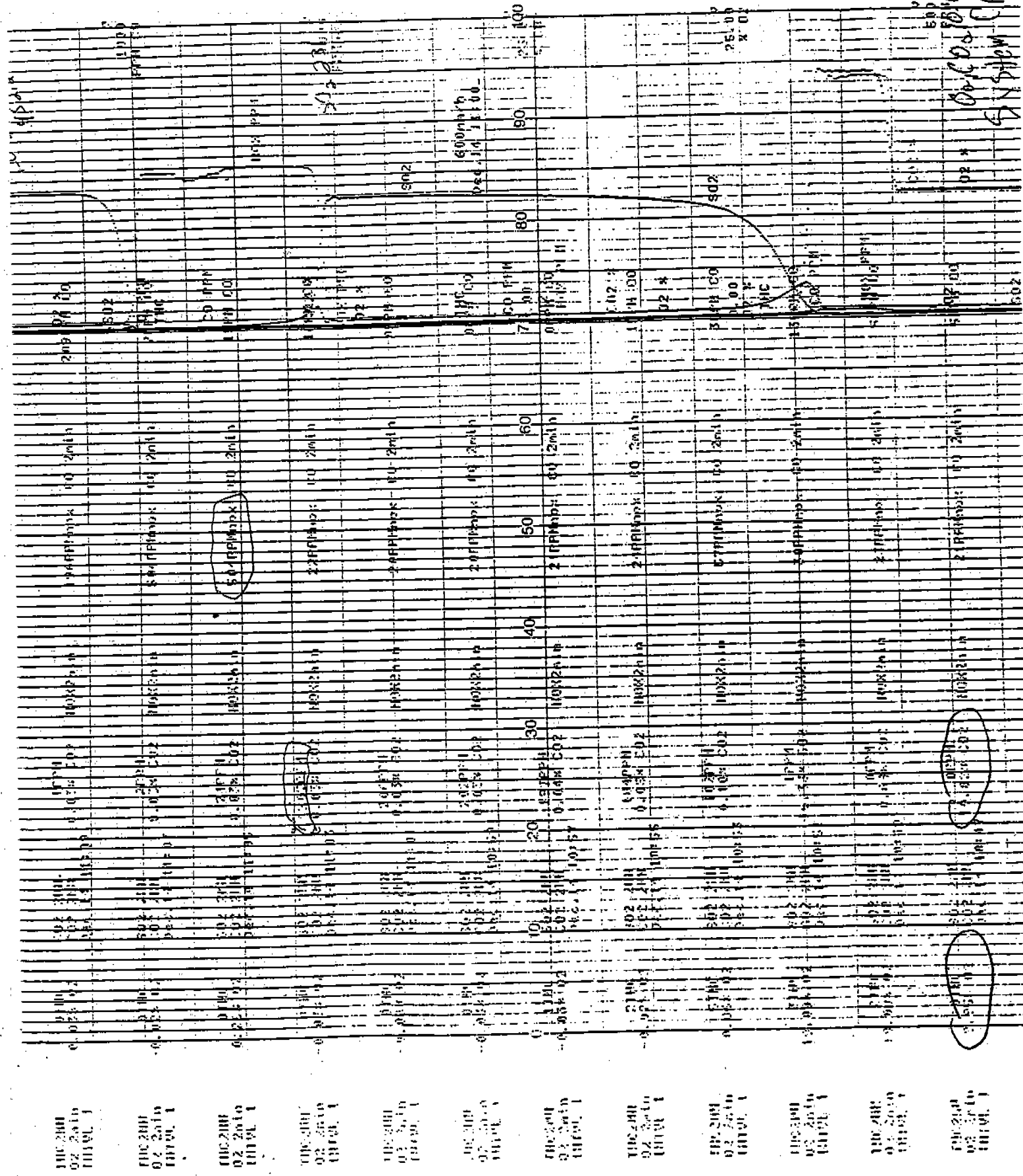
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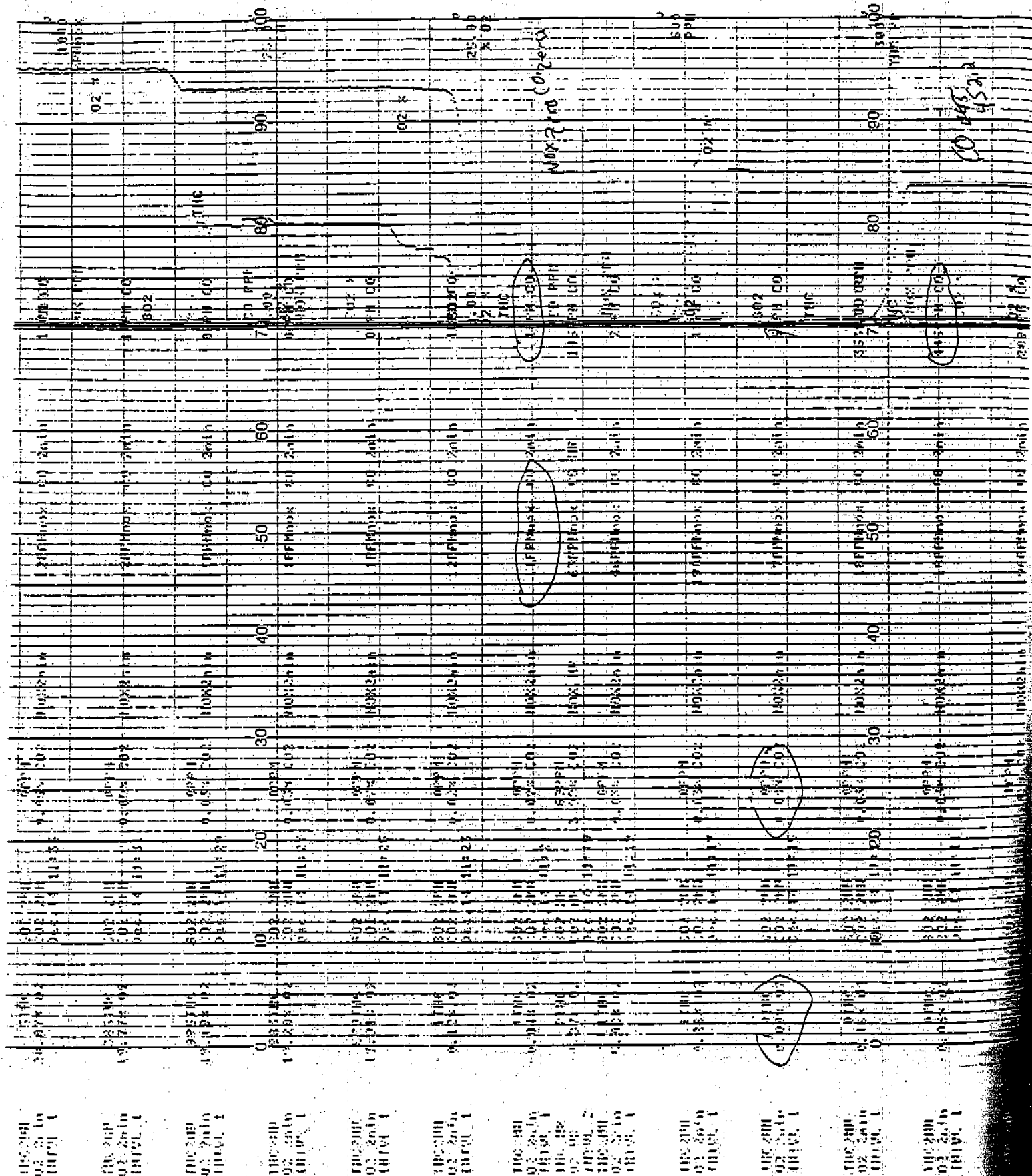
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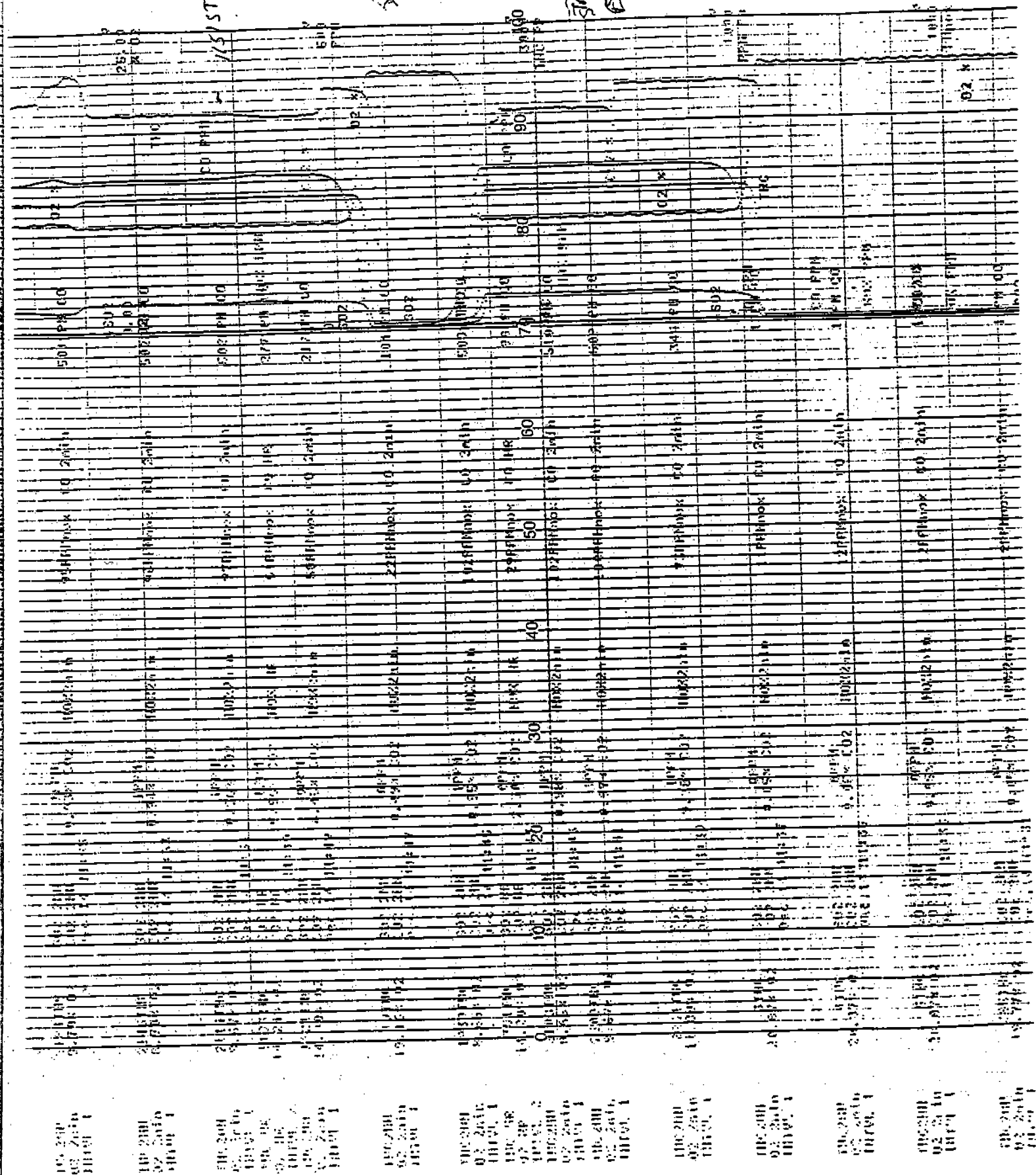
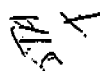
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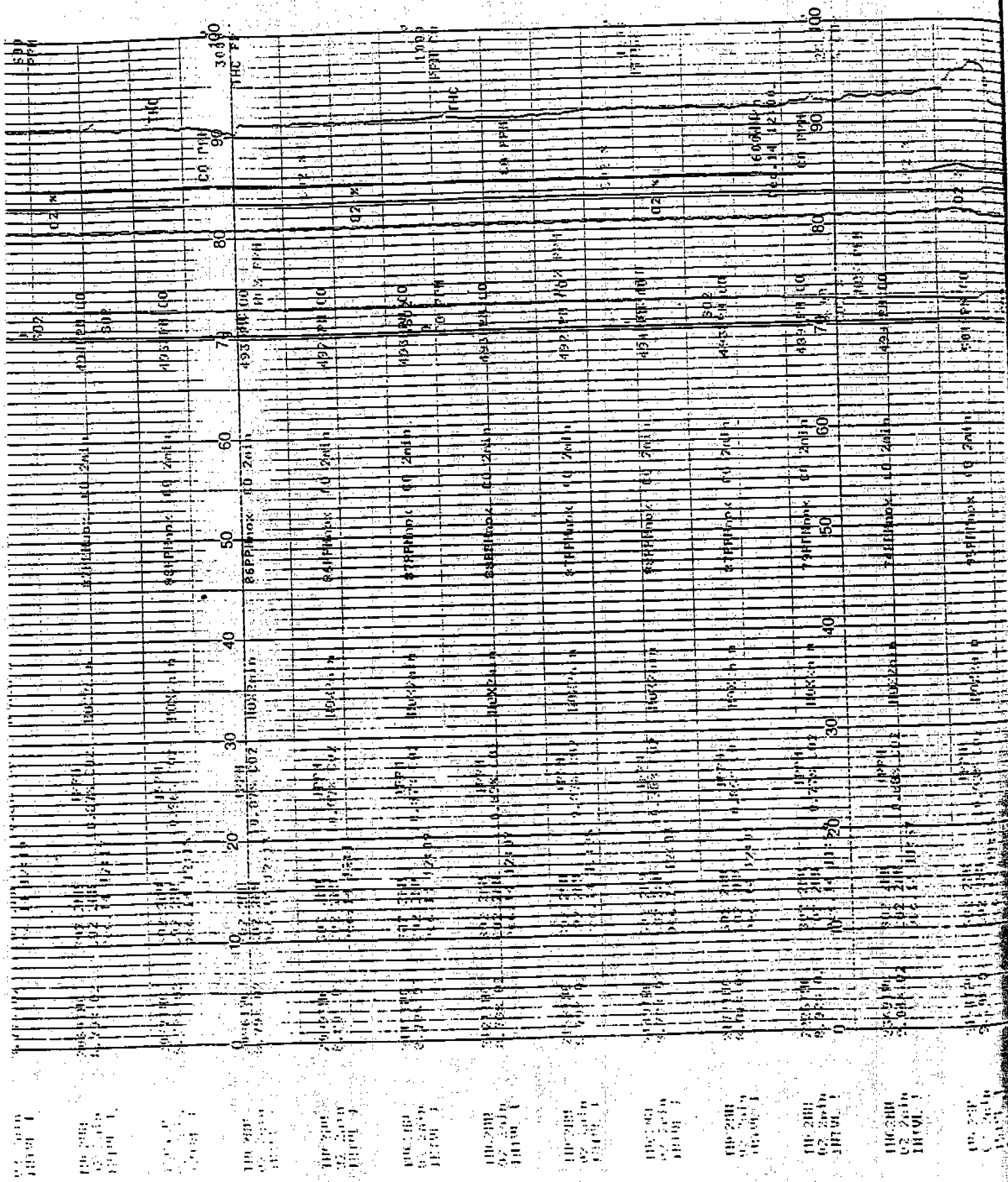
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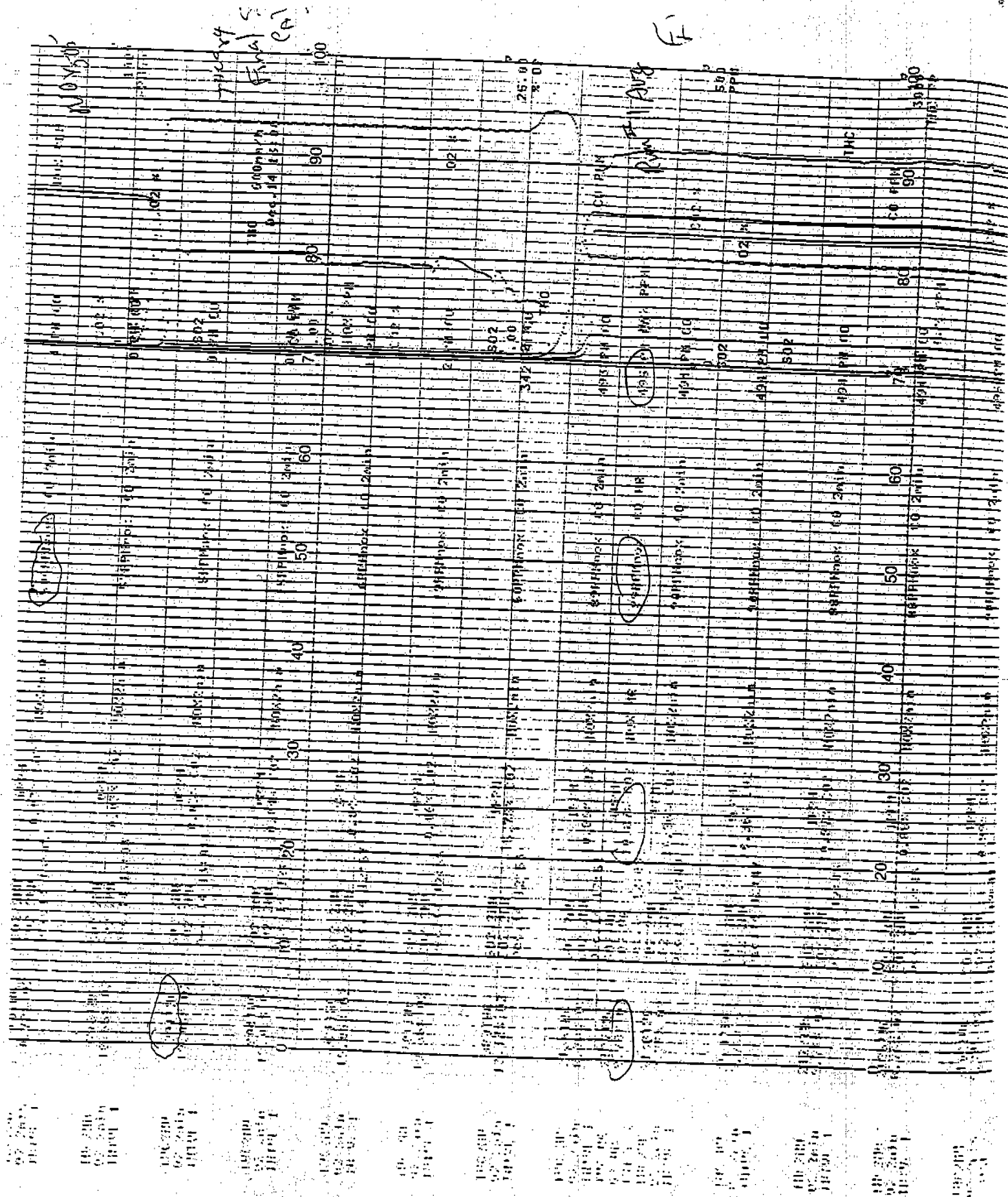
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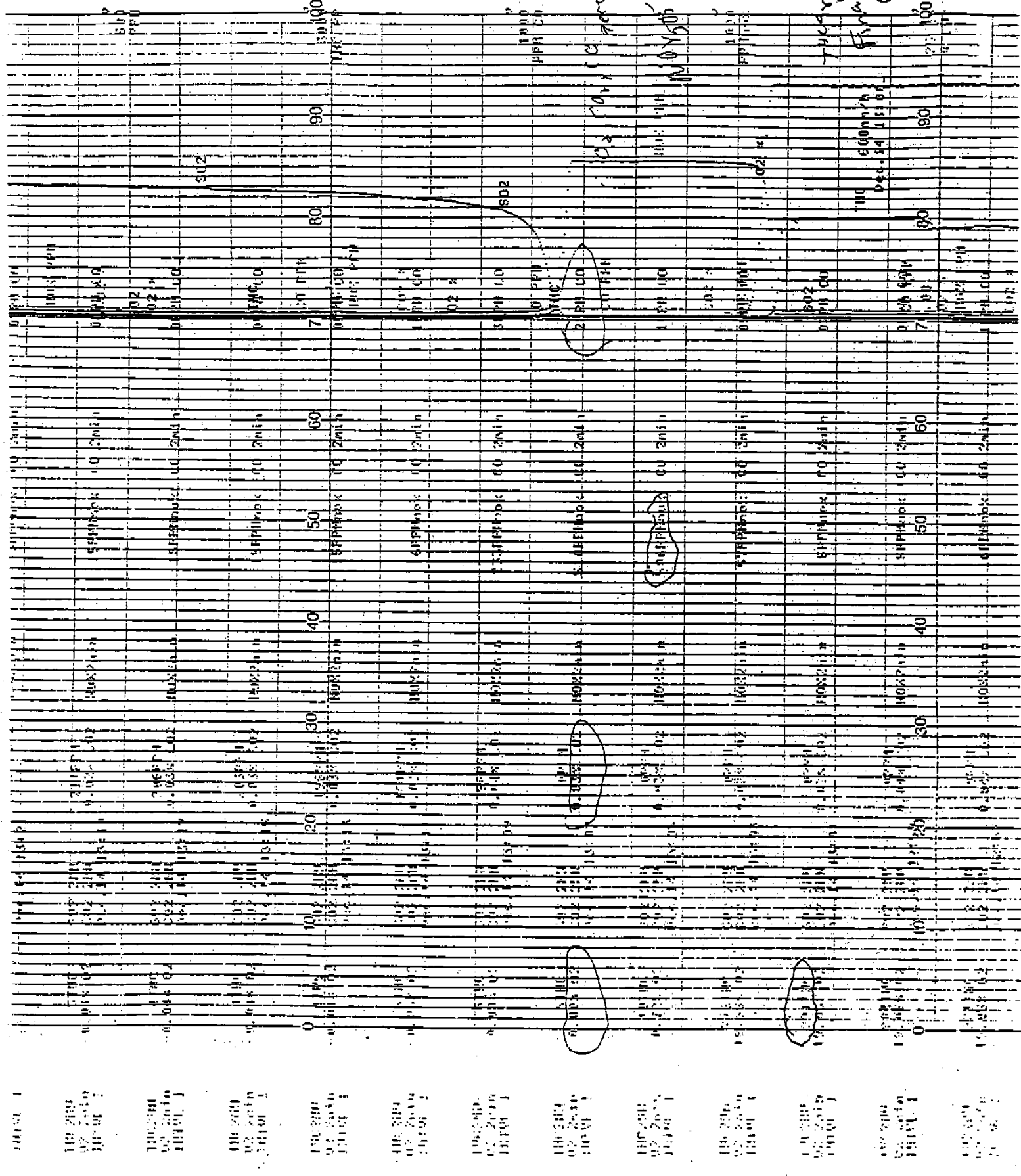
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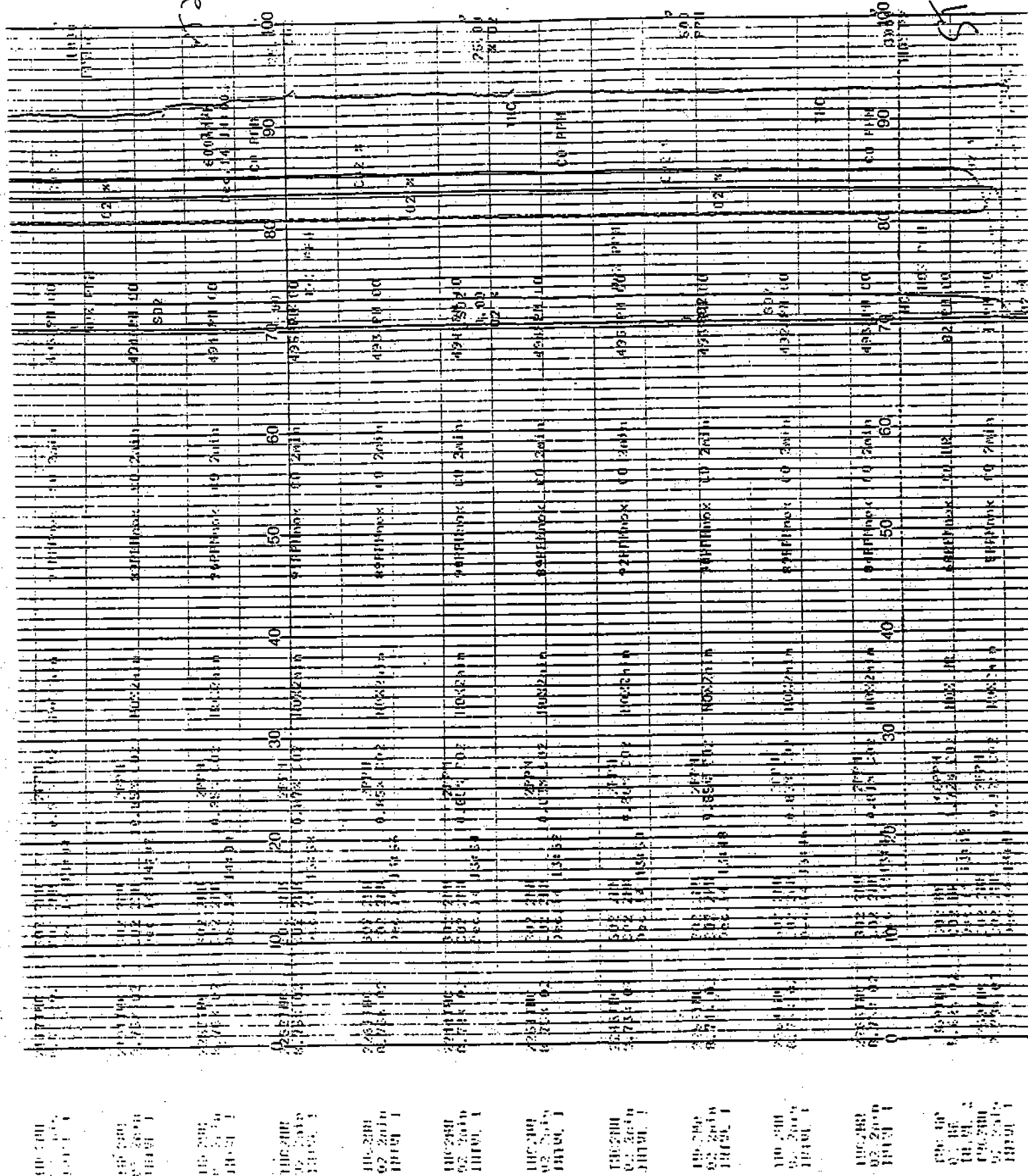
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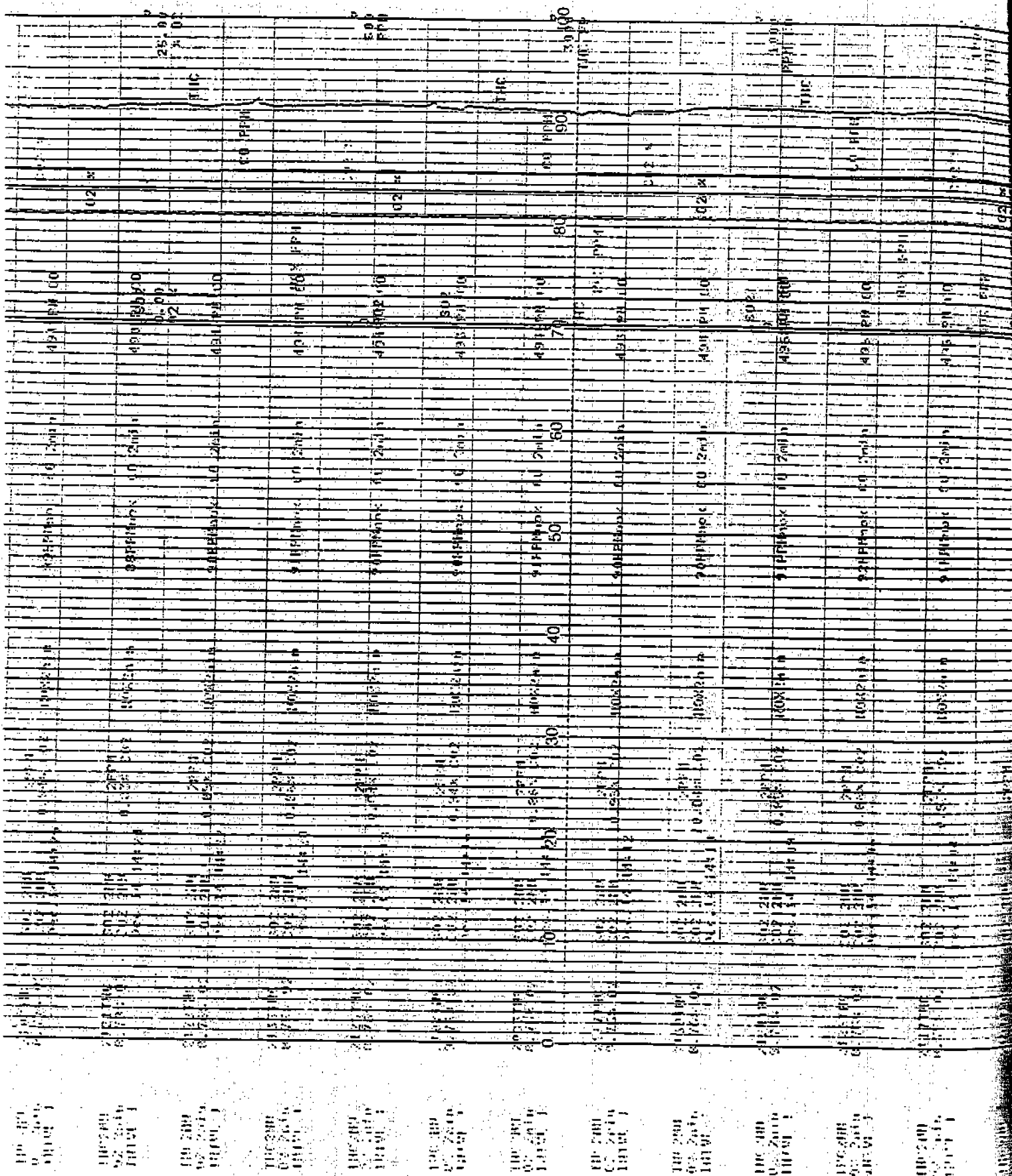
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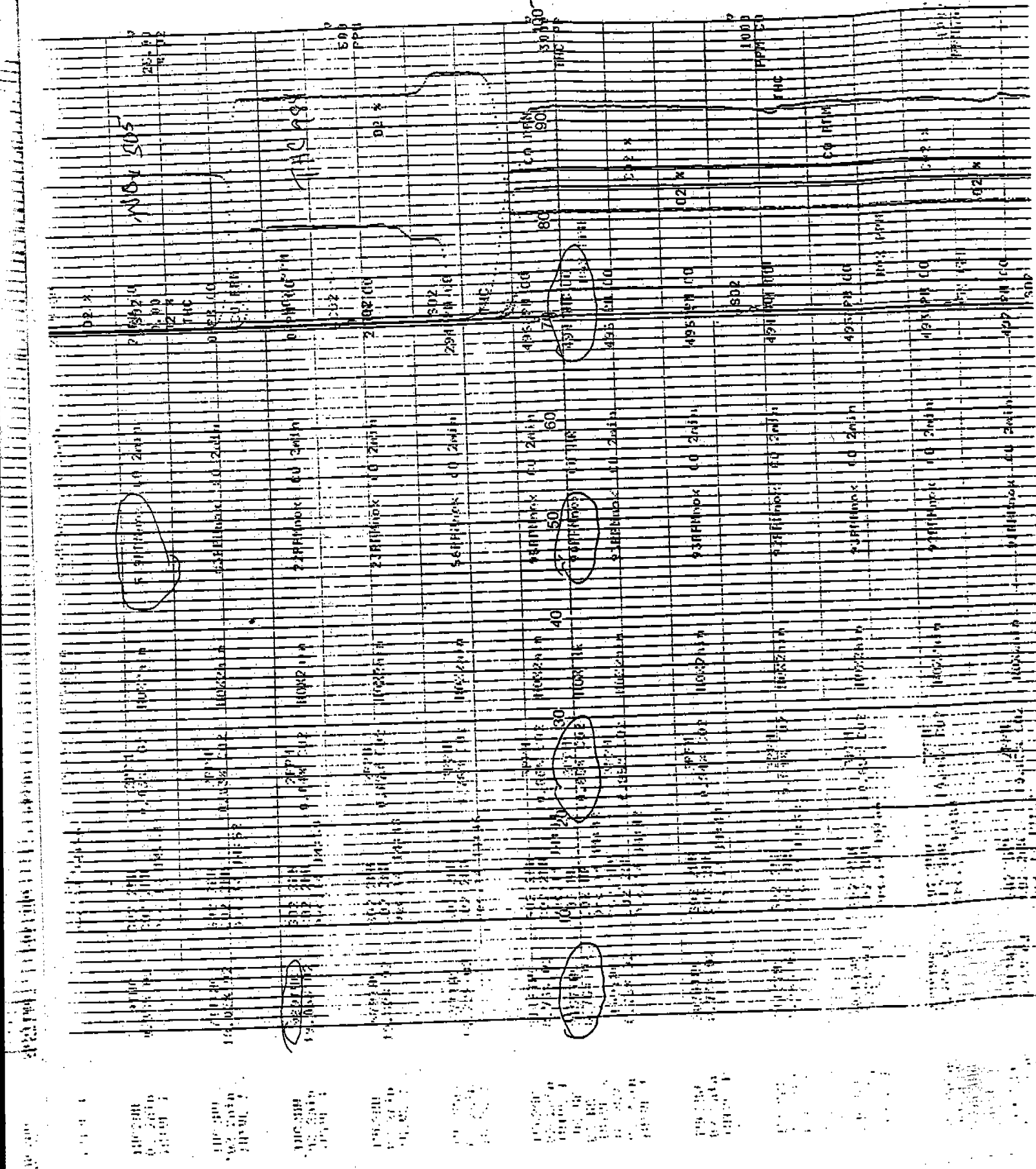
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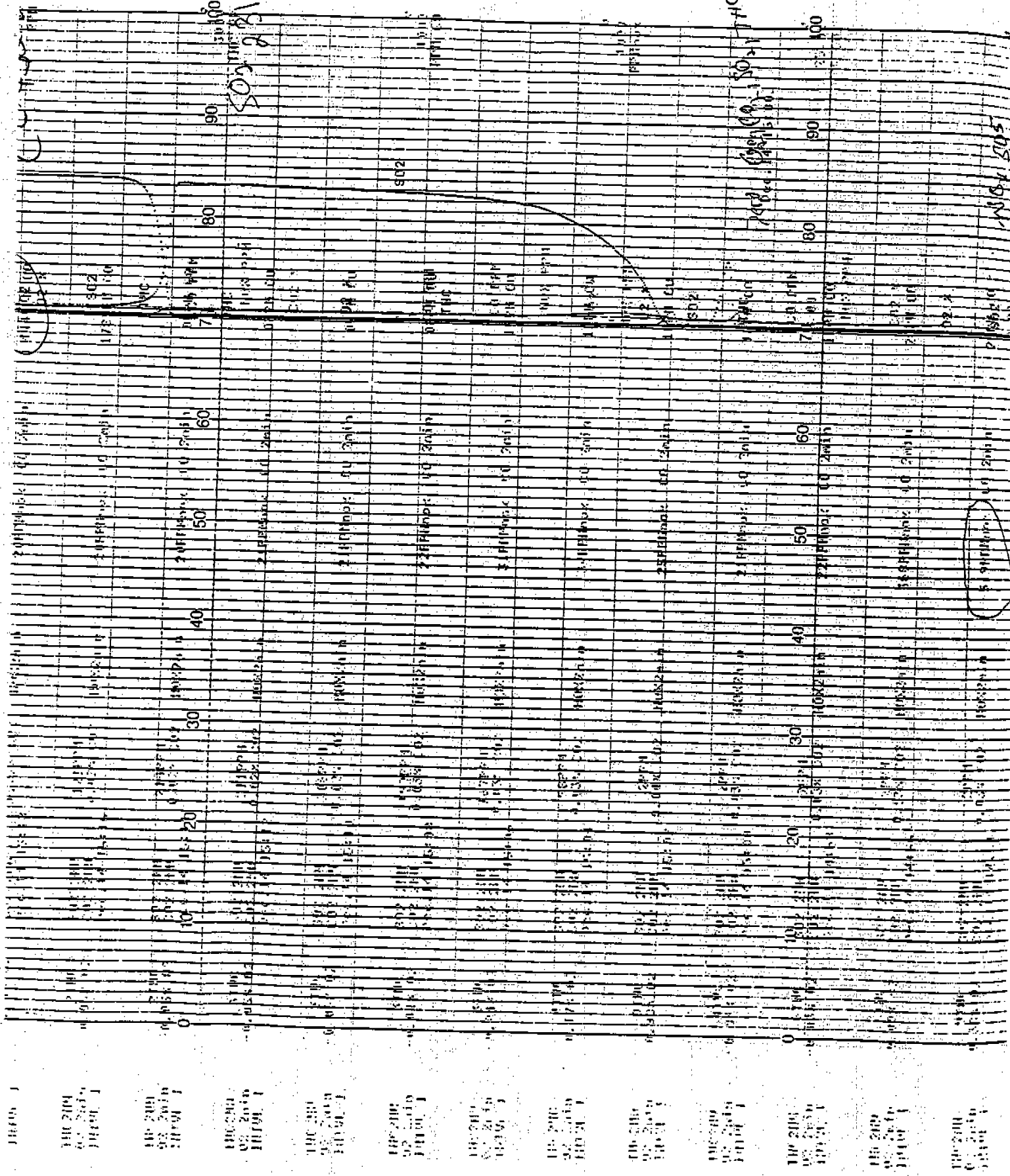
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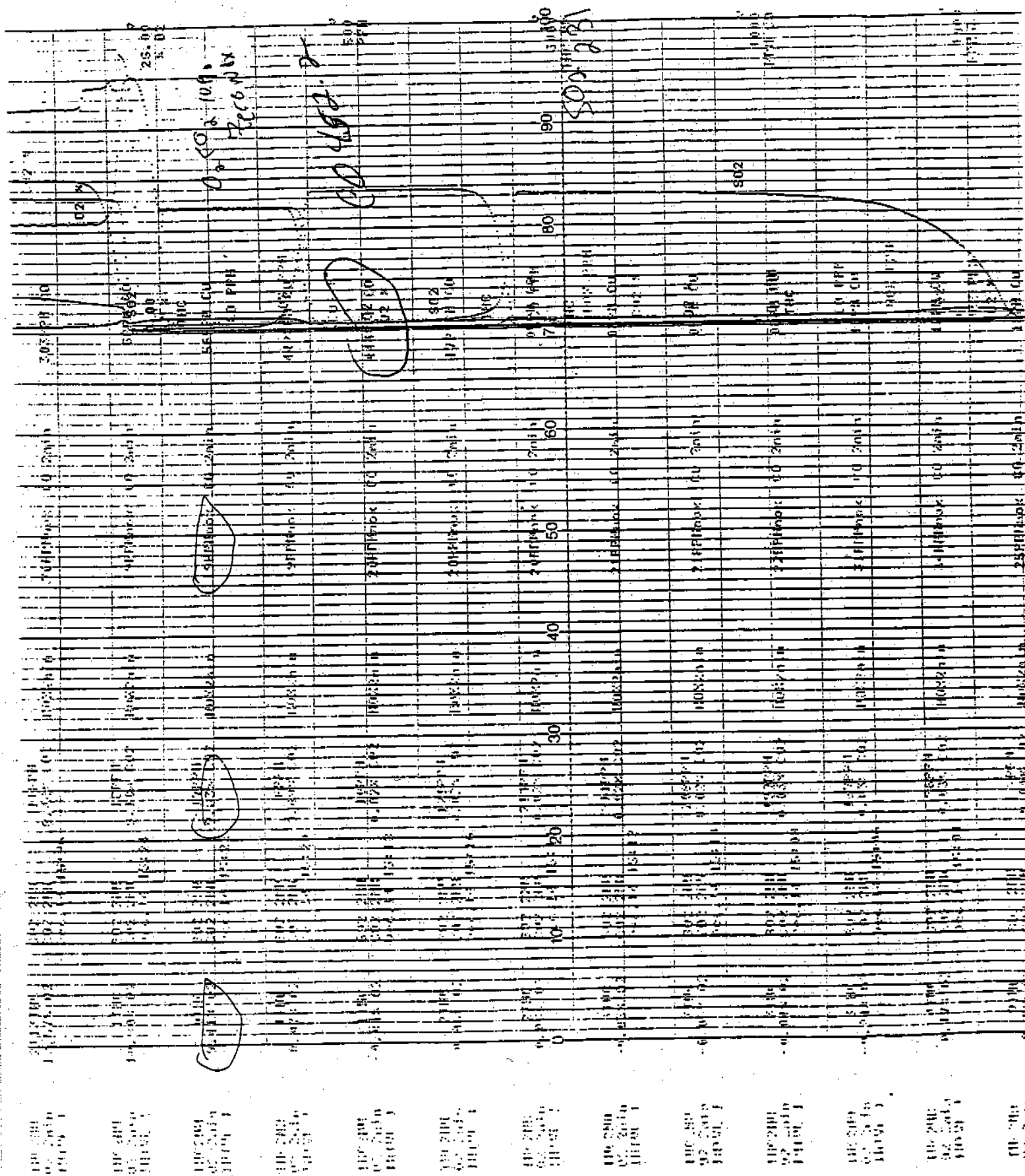
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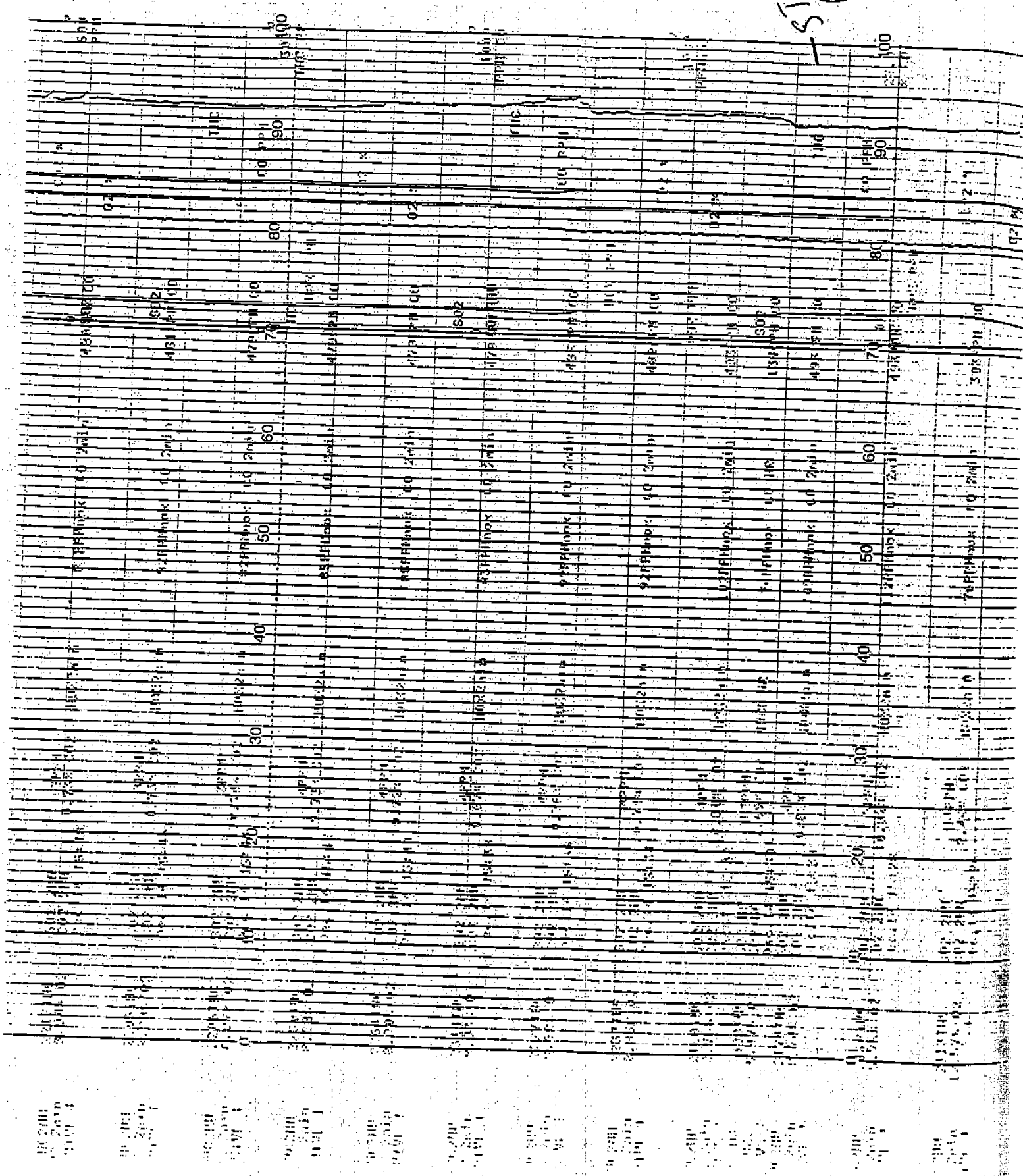


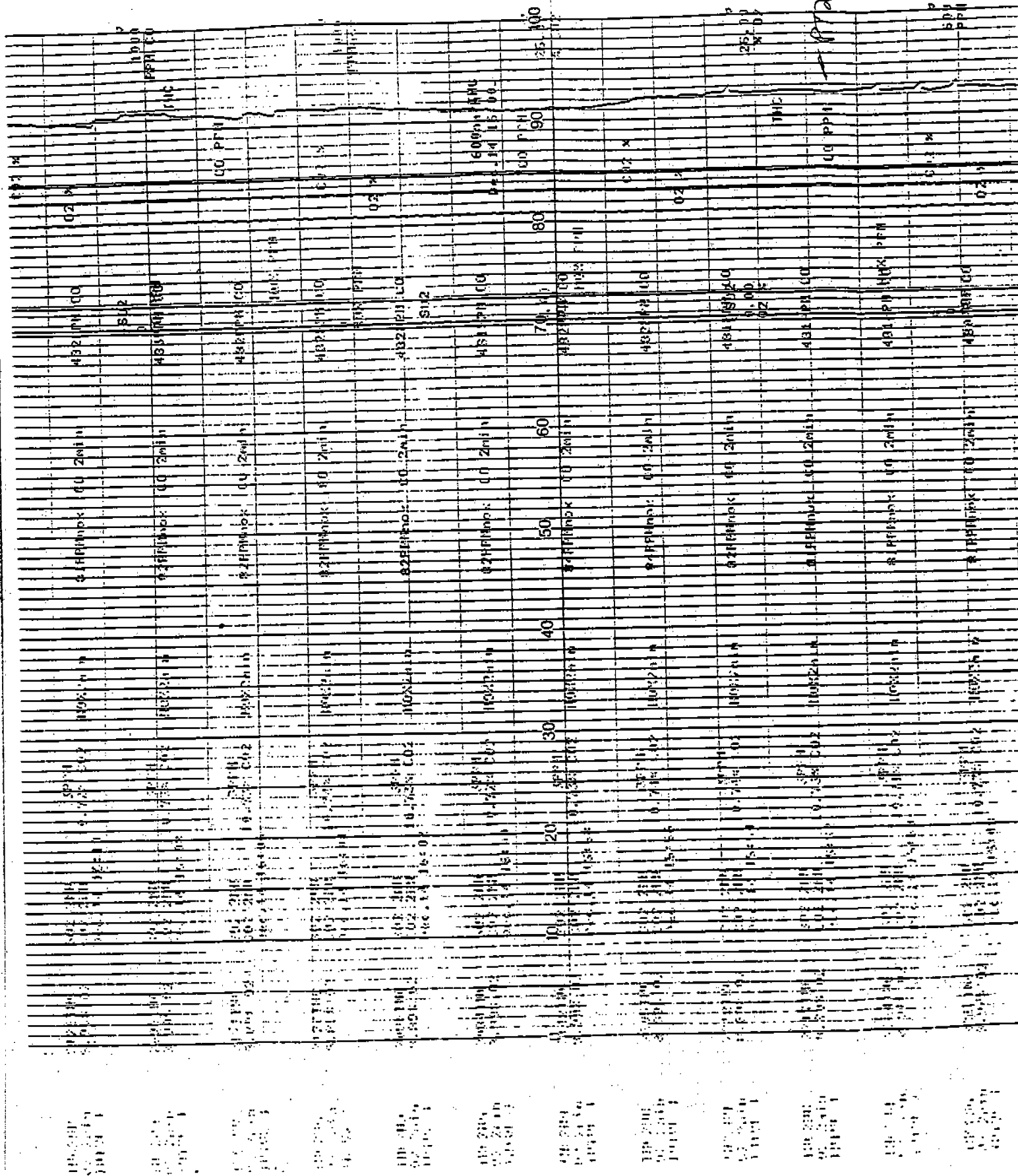


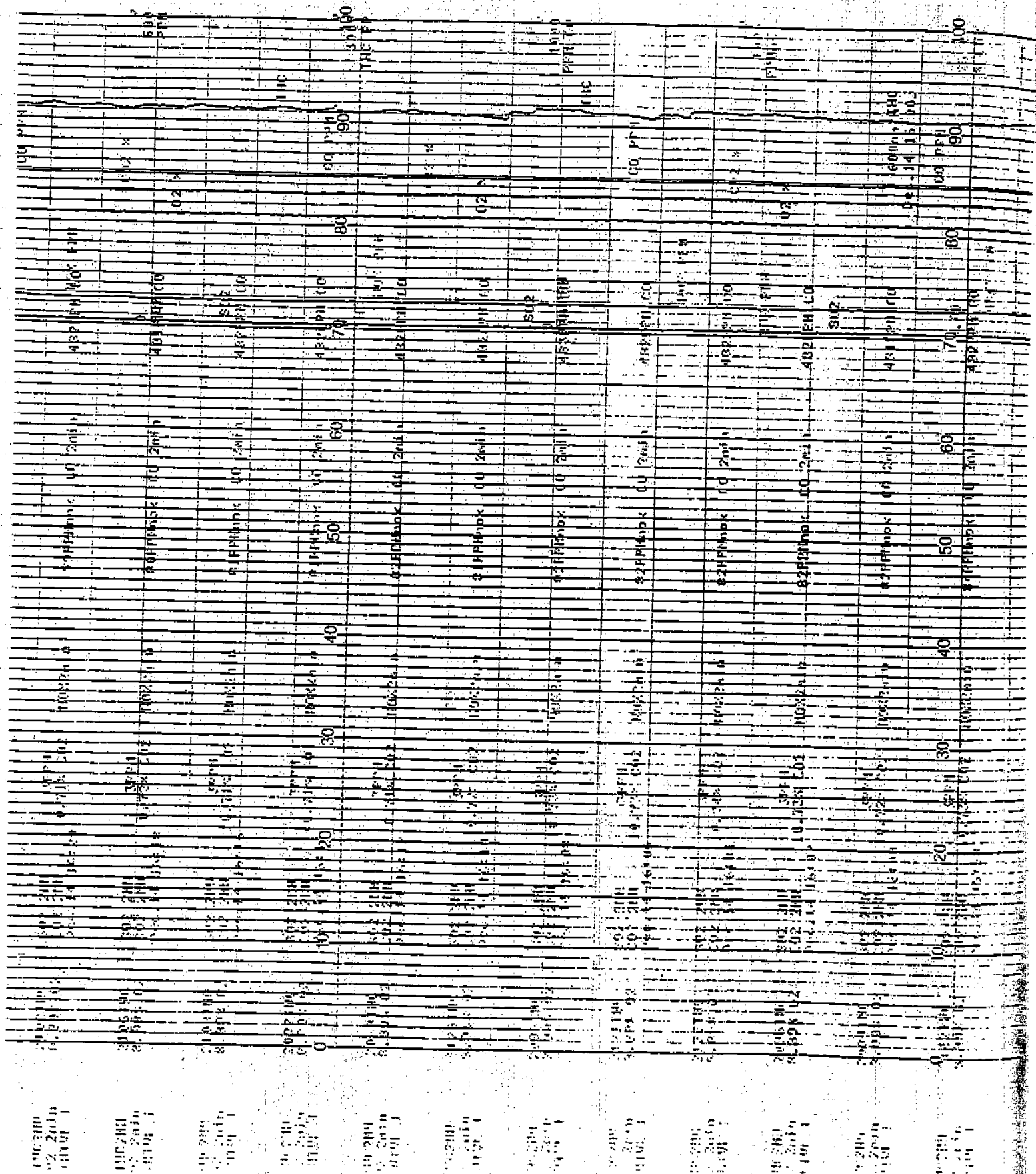


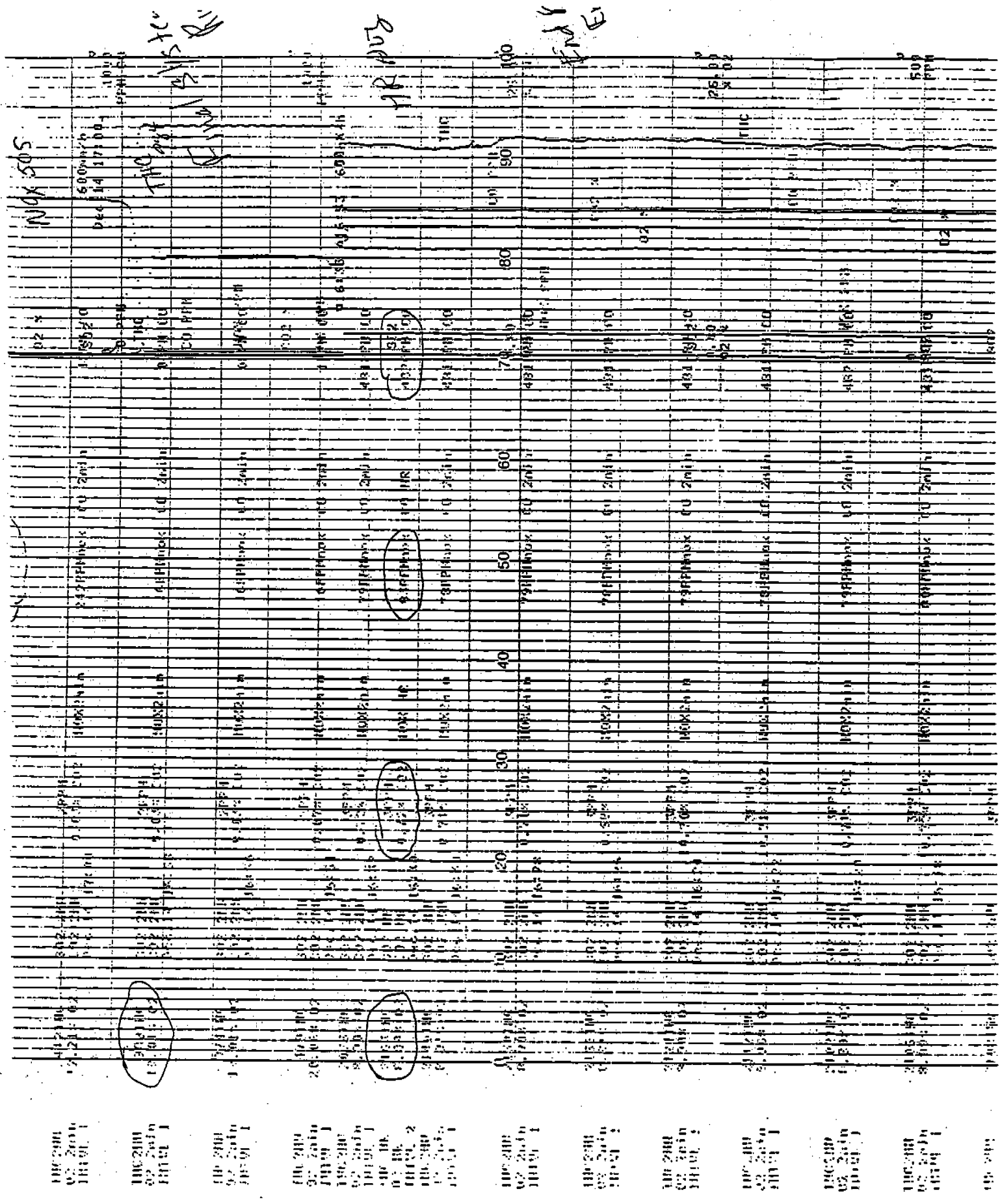


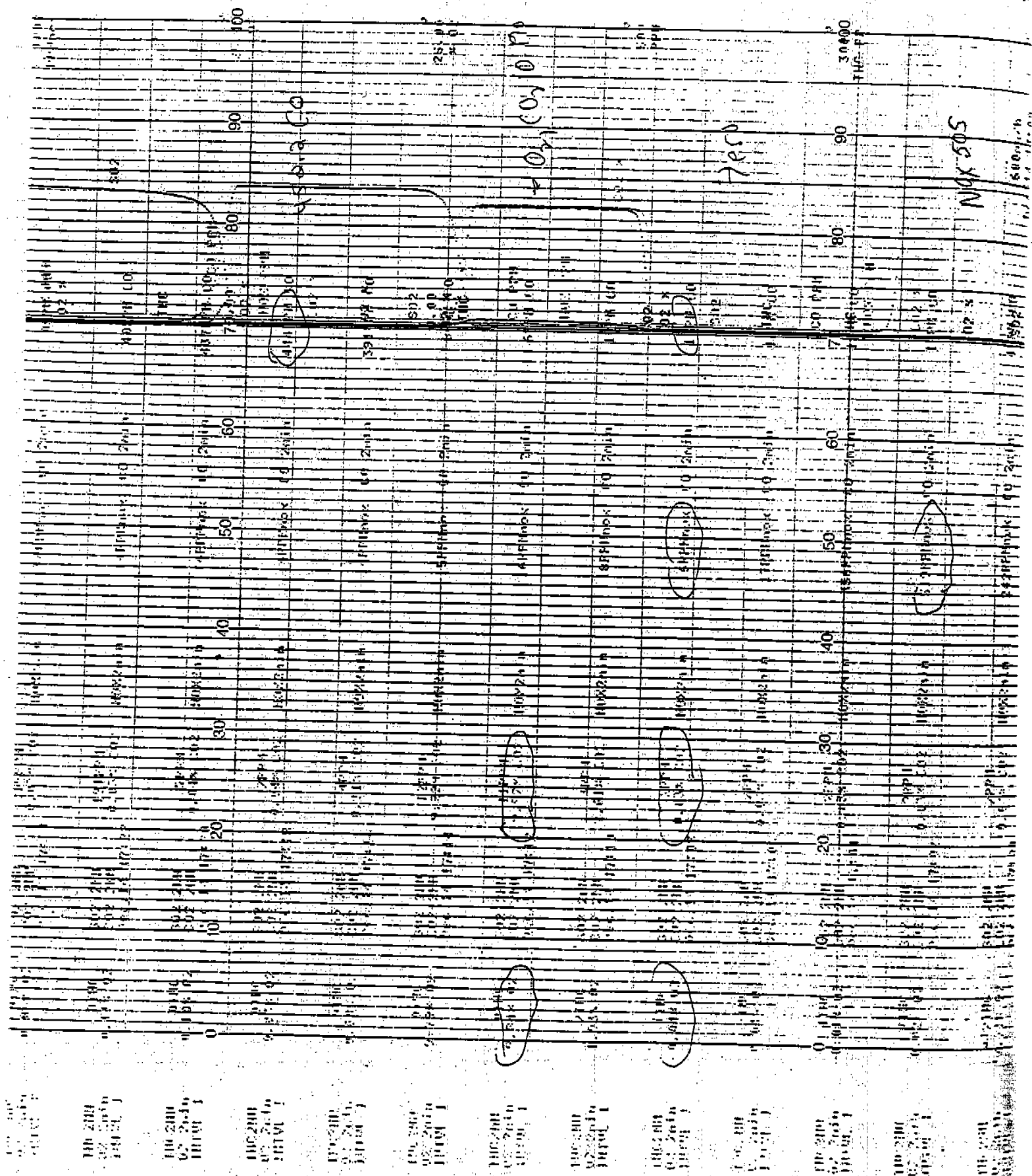
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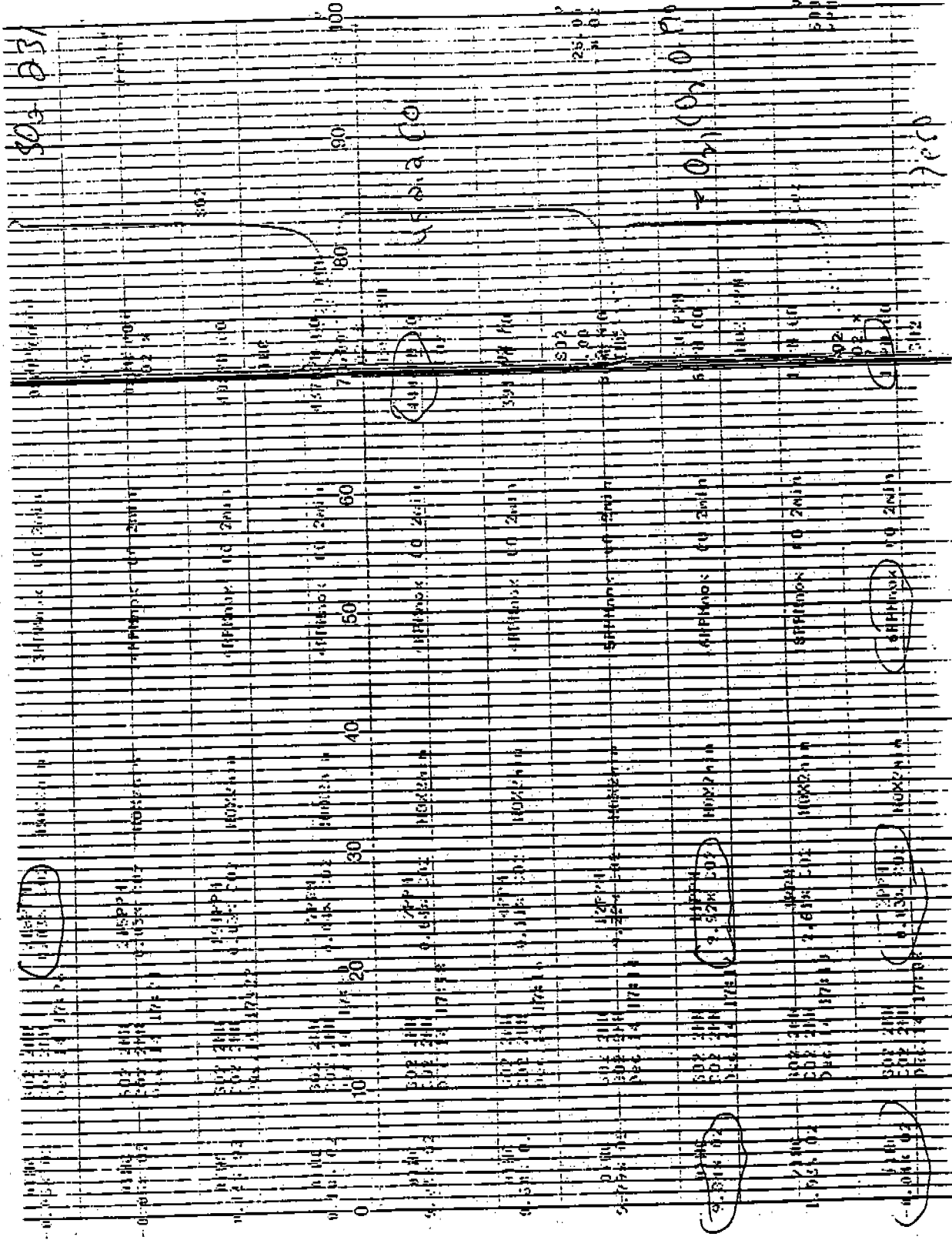














Scott Specialty Gases, Inc.

6141 EASTON ROAD, P.O. BOX 310, PLUMSTEADVILLE, PA 18949-0310

(215) 766-8861 FAX: (215) 766-0320

CERTIFICATE OF ANALYSIS: EPA PROTOCOL GAS

Customer

Trc Environmental
Boott Mills South
Foot Of John Street
Lowell, MA, 01852

Assay Laboratory

Scott Specialty Gases, Inc.
6141 Easton Road
P.O. Box 310
Plumsteadville, PA 18949-0310

Purchase Order T01497

Scott Project # 01-51034-001

ANALYTICAL INFORMATION

Certified to exceed the minimum specifications of EPA Protocol 1 Procedure #G1, Section Number 3.0.4

Cylinder Number ALM040160

Certification Date

11-30-93

Expiration Date

05-15-94

Cylinder Pressure 1900 psig

Previous Certification Dates

None

ANALYZED CYLINDER

Components

Carbon dioxide
Carbon monoxide
Oxygen
Balance Gas Nitrogen

Certified Concentration

4.97 %

6.98 ppm

4.98 %

Analytical Uncertainty*

±1% NIST Directly Traceable

±2% NIST Directly Traceable

±1% NIST Directly Traceable

*Analytical uncertainty is inclusive of usual known error sources which at least includes reference standard error & precision of the measurement processes.

REFERENCE STANDARD

Type

Expiration Date

Cylinder Number

Concentration

NIRM1675

09-28-93

ALM032657

14.01 % CO₂ in N₂

GMIS

01-22-93

ALM018741

15.1 ppm CO in N₂

NIRM2658

05-15-94

ALM015517

9.56 % O₂ in N₂

INSTRUMENTATION

Instrument/Model/Serial #

Last Date Calibrated

Analytical Principle

CO₂: Horiba/AIA23/8505580523

10-22-93

NDIR

CO: Horiba/FA510A/474091

11-20-93

NDIR

O₂: Beckman 755/2002452

10-04-93

Paramagnetic

ANALYZER READINGS

(Z=Zero Gas R=Reference Gas T=Test Gas r=Correlation Coefficient)

Components

First Triad Analysis

Second Triad Analysis

Calibration Curve

Carbon dioxide

Date: 11-23-93 Response Units: Volts
Z1=0.0000 R1=0.5280 T1=0.4140
R2=0.5270 Z2=0.0000 T2=0.4130
Z3=0.0000 T3=0.4140 R3=0.5270
Avg. Conc. of Cust. Cyl. 4.97 %

Date: 11-30-93 Response Units: Volts
Z1=0.0000 R1=0.6250 T1=0.5740
R2=0.3280 Z2=0.0000 T2=0.5780
Z3=0.0000 T3=0.5740 R3=0.6250
Avg. Conc. of Cust. Cyl. 6.97 ppm

Concentration = $A + Bx + Cx^2 + Dx^3 + Ex^4$
 $r = 0.99999$ NIRM1675
Constants: $A = 4.6901E-04$
 $B = 1.1185E+01$ $C = 2.8934E+00$
 $D = 1.1875E+01$ $E = 0.0000E+00$

Carbon monoxide

Date: 11-20-93 Response Units: Volts
Z1=0.0000 R1=0.5260 T1=0.5390
R2=0.5270 Z2=0.0000 T2=0.5610
Z3=0.0000 T3=0.5600 R3=0.5300
Avg. Conc. of Cust. Cyl. 6.98 ppm

Date: 11-30-93 Response Units: Volts
Z1=0.0000 R1=0.6250 T1=0.5740
R2=0.3280 Z2=0.0000 T2=0.5780
Z3=0.0000 T3=0.5740 R3=0.6250
Avg. Conc. of Cust. Cyl. 6.97 ppm

Concentration = $A + Bx + Cx^2 + Dx^3 + Ex^4$
 $r = 0.99999$
Constants: $A = 0.0000E+00$
 $B = 0.0000E+00$ $C = 0.0000E+00$
 $D = 0.0000E+00$ $E = 0.0000E+00$

Oxygen

Date: 11-19-93 Response Units: Volts
Z1=0.0000 R1=0.9338 T1=0.4674
R2=0.9334 Z2=0.0000 T2=0.4859
Z3=0.0000 T3=0.4456 R3=0.9332
Avg. Conc. of Cust. Cyl. 4.98 %

Date: 11-30-93 Response Units: Volts
Z1=0.0000 R1=0.6250 T1=0.5740
R2=0.3280 Z2=0.0000 T2=0.5780
Z3=0.0000 T3=0.5740 R3=0.6250
Avg. Conc. of Cust. Cyl. 6.97 ppm

Concentration = $A + Bx + Cx^2 + Dx^3 + Ex^4$
 $r = 0.99999$ NIRM2658
Constants: $A = 7.5199E-03$
 $B = 1.0207E+01$ $C = 0.0000E+00$
 $D = 0.0000E+00$ $E = 0.0000E+00$

Special Notes

Walter Sath
Analyst Walter Sath



Scott Specialty Gases, Inc.

2330 HAMILTON BOULEVARD SOUTH PLAINFIELD NJ 07080 (908)754-7700 FAX:(908)754-7303

CERTIFICATE OF ANALYSIS: EPA PROTOCOL GAS

Customer
TRC ENVIRONMENTAL
Boott Mills South
Foot of John Street
Lowell MA 01852
Attn.: CAREN O'BRIEN

Assay Laboratory
Scott Specialty Gases
2330 Hamilton Blvd
South Plainfield NJ 07080

Purchase order T01497
Scott Project #0723455

ANALYTICAL INFORMATION

Certified to exceed the minimum specifications of EPA Protocol 1 Procedure #G1 Section Number 3.0.4

Cylinder Number 1L2110
Cylinder Pressure 2000psig

Certification Date 10-25-1993
Previous Certification Dates

Expiration Date 4-25-1994

ANALYZED CYLINDER

Components

CARBON DIOXIDE
CARBON MONOXIDE

Certified Concentration

10.1%
10.2ppm

Analytical Uncertainty*

+/-1%NIST Directly Traceable
+/-1%NIST Directly Traceable

Nitrogen

Balance

*Analytical uncertainty is inclusive of usual known error sources which at least includes reference standard error & precision of the measurement process

REFERENCE STANDARD

Type **Expiration Date**
CRM1675 **03/20/94**
CRM1677 **wait**

Cylinder Number
ALM001140
AAL9208

Concentration
14.02 %CO₂ in N₂
9.9 ppmCO in N₂

INSTRUMENTATION

Instrument/Model/Serial#
CO₂: Varian-3700-31608928
CO: Ecolyzer 2000 - 1709

Date Last Calibrated
09/03/1993
08/01/1993

Analytical Principle
GC TCD
Electrochemical

ANALYZER READINGS (Z=Zero Gas R=Reference Gas T=Test Gas r=Correlation Coefficient)

Components	First Triad Analysis	Second Triad Analysis	Calibration Curve
CARBON DIOXIDE	Date: 10-25-1993 Response units: % Z1=0 R1= 14.02 T1=10.1 R2= 14.02 Z2=0 T2=10.1 Z3=0 T3=10.1 R3= 14.02 Ave. Conc. of Cust. Cyl = 10.1		Concentration = $A + Bx + Cx^2 + Dx^3 + Ex^4$ $r = 0.9999919$ Constants: $A = -3.7268E-02$ $B = 5.7325E-05$ $C =$ $D =$ $E =$
CARBON MONOXIDE	Date: 10-11-1993 Response units: ppm Z1=0 R1= 9.9 T1=10.3 R2= 9.9 Z2=0 T2=10.3 Z3=0 T3=10.3 R3= 9.9 Ave. Conc. of Cust. Cyl = 10.3	Date: 10-25-1993 Response units: ppm Z1=0 R1= 9.9 T1=10.2 R2= 9.9 Z2=0 T2=10.1 Z3=0 T3=10.2 R3= 9.9 Ave. Conc. of Cust. Cyl = 10.2	Concentration = $A + Bx + Cx^2 + Dx^3 + Ex^4$ $r = 0.9999961$ Constants: $A = 4.2212E-01$ $B = 1.0308E-03$ $C =$ $D =$ $E =$

Special Notes



Scott Specialty Gases, Inc.

2330 HAMILTON BOULEVARD SOUTH PLAINFIELD NJ 07080 (908)754-7700 FAX:(908)754-7303

CERTIFICATE OF ANALYSIS: EPA PROTOCOL GAS

Customer

TRC ENVIRONMENTAL
Boott Mills South
Foot of John Street
Lowell MA 01852
Attn.: CAREN O'BRIEN

Assay Laboratory

Scott Specialty Gases
2330 Hamilton Blvd
South Plainfield NJ 07080

Purchase order T01497
Scott Project #0723455

ANALYTICAL INFORMATION

Certified to exceed the minimum specifications of EPA Protocol 1 Procedure #G1 Section Number 3.0.4

Cylinder Number 1L2110
Cylinder Pressure 2000psig

Certification Date 10-25-1993
Previous Certification Dates

Expiration Date 4-25-1994

ANALYZED CYLINDER

Components

OXYGEN
SULFUR DIOXIDE

Certified Concentration

10.1%
16.3ppm

Analytical Uncertainty*

+/-1%NIST Directly Traceable
+/-1%NIST Directly Traceable

Nitrogen

Balance

*Analytical uncertainty is inclusive of usual known error sources which at least includes reference standard error & precision of the measurement processes

REFERENCE STANDARD

Type

CRM2658
CRM1693

Expiration Date

05/14/94
09/28/94

Cylinder Number

ALM017572
ALM024299

Concentration

9.56 %O2 in N2
47.2 ppmSO2 in N2

INSTRUMENTATION

Instrument/Model/Serial#

O2: Varian-3700-31608928
SO2: Wilks Miran-1A-1047

Date Last Calibrated

09/14/1993
10-25-1993

Analytical Principle

GC TCD
Infra Red Spectrophotometry

ANALYZER READINGS (Z=Zero Gas R=Reference Gas T=Test Gas r=Correlation Coefficient)

Components

First Triad Analysis

Second Triad Analysis

Calibration Curve

OXYGEN

Date: 10-25-1993 Response units: %
Z1=0 R1= 9.56 T1=10.1
R2= 9.56 Z2=0 T2=10.2
Z3=0 T3=10.1 R3= 9.56
Ave. Conc. of Cust. Cyl = 10.1

Concentration = $A + Bx + Cx^2 + Dx^3 + Ex^4$
 $r = 0.9999926$
Constants: A = 1.5815E-01
B = 4.7835E-05 C =
D = E =

SULFUR DIOXIDE

Date: 10-13-1993 Response units: ppm
Z1=0 R1= 47.2 T1=16.4
R2= 47.2 Z2=0 T2=16.5
Z3=0 T3=16.4 R3= 47.2
Ave. Conc. of Cust. Cyl = 4

Date: 10-25-1993 Response units: ppm
Z1=0 R1= 47.2 T1=16.2
R2= 47.2 Z2=0 T2=16.2
Z3=0 T3=16.2 R3= 47.2
Ave. Conc. of Cust. Cyl = 4042

Concentration = $A + Bx + Cx^2 + Dx^3 + Ex^4$
 $r = .9999968$
Constants: A = -8.617049
B = .7894195 C = 2.9886E-04
D = -4.3646E-07 E =

Special Notes



Scott Specialty Gases, Inc.

2330 HAMILTON BOULEVARD SOUTH PLAINFIELD NJ 07080 (908)754-7700 FAX:(908)754-7303

CERTIFICATE OF ANALYSIS: EPA PROTOCOL GAS

Customer
TRC ENVIRONMENTAL
Boott Mills South
Foot of John Street
Lowell MA 01852
Attn.: CAREN O'BRIEN

Assay Laboratory
Scott Specialty Gases
2330 Hamilton Blvd
South Plainfield NJ 07080

Purchase order T01497
Scott Project #0723455

ANALYTICAL INFORMATION

Certified to exceed the minimum specifications of EPA Protocol 1 Procedure #G1 Section Number 3.0.4

Cylinder Number ALM015679
Cylinder Pressure 2000psig

Certification Date 10-25-1993
Previous Certification Dates

Expiration Date 4-25-1994

ANALYZED CYLINDER

Components

CARBON DIOXIDE
CARBON MONOXIDE

Certified Concentration

19.9%
19.2ppm

Analytical Uncertainty*

+/-1%NIST Directly Traceable
+/-1%NIST Directly Traceable

Nitrogen

Balance

*Analytical uncertainty is inclusive of usual known error sources which at least includes reference standard error & precision of the measurement processes

REFERENCE STANDARD

Type **Expiration Date**
CRM1675 03/20/94
SRM2635A 03/22/95

Cylinder Number
ALM001140
FF30354

Concentration
14.02 %CO₂ in N₂
24 ppmCO in N₂

INSTRUMENTATION

Instrument/Model/Serial#
CO₂: Varian-3700-31608928
CO: Ecolyzer 2000-1709

Date Last Calibrated
09/03/1993
08/01/1993

Analytical Principle
GC TCD
Electrochemical

ANALYZER READINGS (Z=Zero Gas R=Reference Gas T=Test Gas r=Correlation Coefficient)

Components	First Triad Analysis	Second Triad Analysis	Calibration Curve
CARBON DIOXIDE	Date: 10-25-1993 Response units: % Z1=0 R1= 14.02 T1=19.9 R2= 14.02 Z2=0 T2=19.9 Z3=0 T3=19.9 R3= 14.02 Ave. Conc. of Cust. Cyl. = 19.9		Concentration = $A + Bx + Cx^2 + Dx^3 + Ex^4$ $r = 0.9999919$ Constants: A = -3.7268E-02 B = 5.7325E-05 C = D = E =
CARBON MONOXIDE	Date: 10-11-1993 Response units: ppm Z1=0 R1= 24 T1=19.1 R2= 24 Z2=0 T2=19.1 Z3=0 T3=19.1 R3= 24 Ave. Conc. of Cust. Cyl. = 19.1	Date: 10-25-1993 Response units: ppm Z1=0 R1= 24 T1=19.3 R2= 24 Z2=0 T2=19.3 Z3=0 T3=19.3 R3= 24 Ave. Conc. of Cust. Cyl. = 19.3	Concentration = $A + Bx + Cx^2 + Dx^3 + Ex^4$ $r = 0.9999961$ Constants: A = 4.2212E-01 B = 1.0308E-03 C = D = E =

Special Notes



Scott Specialty Gases, Inc.

2330 HAMILTON BOULEVARD SOUTH PLAINFIELD NJ 07080 (908)754-7700 FAX:(908)754-7303

CERTIFICATE OF ANALYSIS: EPA PROTOCOL GAS

Customer
TRC ENVIRONMENTAL
Boott Mills South
Foot of John Street
Lowell MA 01852
Attn.: CAREN O'BRIEN

Assay Laboratory
Scott Specialty Gases
2330 Hamilton Blvd
South Plainfield NJ 07080

Purchase order T01497
Scott Project #0723455

ANALYTICAL INFORMATION

Certified to exceed the minimum specifications of EPA Protocol 1 Procedure #G1 Section Number 3.0.4

Cylinder Number ALM015679
Cylinder Pressure 2000psig

Certification Date 10-25-1993
Previous Certification Dates

Expiration Date 4-25-1994

ANALYZED CYLINDER

Component:

OXYGEN
SULFUR DIOXIDE

Certified Concentration

20.0%
21.1ppm

Analytical Uncertainty*

+/-1%NIST Directly Traceable
+/-1%NIST Directly Traceable

Nitrogen

Balance

*Analytical uncertainty is inclusive of usual known error sources which at least includes reference standard error & precision of the measurement processes

REFERENCE STANDARD

Type Expiration Date
CRM2659 05/14/94
CRM1693 09/28/94

Cylinder Number
ALM017576
ALM024299

Concentration
20.63 %O2 in N2
47.2 ppmSO2 in N2

INSTRUMENTATION

Instrument/Model/Serial#
O2: Varian-3700-31608928
SO2: Wilks Miran-1A-1047

Date Last Calibrated
09/14/1993
10-25-1993

Analytical Principle
GC TCD
Infra Red Spectrophotometry

ANALYZER READINGS (Z=Zero Gas R=Reference Gas T=Test Gas r=Correlation Coefficient)

Components	First Triad Analysis	Second Triad Analysis	Calibration Curve
OXYGEN	Date: 10-25-1993 Response unit: % Z1=0 R1=20.63 T1=20.0 R2=20.63 Z2=0 T2=20.0 Z3=0 T3=20.0 R3=20.63 Ave. Conc. of Cust. Cyl. = 20		Concentration = $A + Bx + Cx^2 + Dx^3 + Ex^4$ $r = 0.9999926$ Constants: A = 1.5815E-01 B = 4.7835E-05 C = D = E =
SULFUR DIOXIDE	Date: 10-11-1993 Response unit: ppm Z1=0 R1=47.2 T1=21.0 R2=47.2 Z2=0 T2=20.9 Z3=0 T3=21.0 R3=47.2 Ave. Conc. of Cust. Cyl. = 21	Date: 10-25-1993 Response unit: ppm Z1=0 R1=47.2 T1=21.2 R2=47.2 Z2=0 T2=21.2 Z3=0 T3=21.2 R3=47.2 Ave. Conc. of Cust. Cyl. = 21.2	Concentration = $A + Bx + Cx^2 + Dx^3 + Ex^4$ $r = .9999968$ Constants: A = -8.617049 B = .7894195 C = 2.9886E-04 D = -4.3646E-07 E =

Special Notes

SCOTT Specialty Gases

2330 Hamilton Blvd South Plainfield NJ
PHONE 908-754-7700 FAX 908-754-7303

CERTIFICATION OF ANALYSIS-EPA PROTOCOL

Date Shipped 07-15-1992
certified per protocol#1 Procedure 3.0.4-G1
cylinder # ALM027031 ✓

MINOR
CERT. comp.

sulfur dioxide 25 ppm +/- 1%

Our Project 0716175

REFERENCE STD
CRM/CRM num

CYL. num
ALH007008 1001

Top Pressure 2000psi

MAKE/ model
GAS ANALYZER

STD conc. 454 ppm
LAST cal. 01.01.94

Your P.O. 22436
ANAL prin.
Mettler Hirsch-1A-1047-Infra Red Spectrophotometry

EXPIRES 1-15-1994

BALANCE Nitrogen

ANALYZER READINGS

First Analysis

Second Analysis

Sulfur Dioxide
all values as ppm

Date: 07-08-1992 Mean test assay 229
Zero= 0 Ref.= 454 Test=229
Ref.= 454 Zero= 0 Test=229
Zero= 0 Ref.= 454 Test=229

Date: 07-15-1992 Mean test assay 232
Zero= 0 Ref.= 454 Test=232
Ref.= 454 Zero= 0 Test=232
Zero= 0 Ref.= 454 Test=232

02/17/94 09:59 FAX 617 246 5452...
02/18/94 15:47 908 754 7303

SCOTT MASS
SCOTT GASES = NJ -- SCOTT MASS

002
002

APPROVED BY *[Signature]*

[Signature]

ANALYST

SCOTT Specialty Gases

APPROVED BY *[Signature]*

SCOTT Specialty Gases

CERTIFICATION OF ANALYSIS-EPA PROTOCOL

Date Shipped 06-29-1993
 certified per protocol #1 procedure 3.0.4-G1
 cylinder # ALM037636
 MINOR
 comp. OERT. CONO. 907ppm/-1% 932ppm/-1%
 Carbon Monoxide
 Sulfur Dioxide
 Our Project 0721482
 REFERENCE STD
 CIL. NUM ALM023748 ALM008672
 num 1000 1002
 OIM/SHM
 num 1000 1002
 STD CONO. 956 ppm 1006 ppm
 MAKE/ model
 LAST cal.
 GAS ANALYZER
 ANAL prin.
 Your P.O. T00636
 Top Pressure 2000psi
 Per. Elm.-01gma 2000-004331001115-4/16/93-00 FID
 Witha Hiran-1A-1027-Infra Red Spectrophotometry

BALANCE Nitrogen
 ANALYZER READINGS
 Component
 Carbon Monoxide
 all values as ppm
 Sulfur Dioxide
 all values as ppm

6-29-1995 (general)
 EXPIRES 12-29-1993 (acid rain)
 Second Analysis
 Date: 06-29-1993
 test assay 950
 Zero 0 Ref. = 956 Test = 956
 Ref. = 956 Zero = 0 Test = 956
 Zero = 0 Test = 956 Ref. = 956
 Date: 06-29-1993
 test assay 933
 Zero 0 Ref. = 1006 Test = 934
 Ref. = 1000 Zero = 0 Test = 933
 Zero = 0 Test = 933 Ref. = 1006

ANALYST Adela sy
 APPROVED BY John O'shea

Scott Specialty Gases
 2330 Hamilton Blvd South Plainfield NJ
 PHONE 908-764-7700 FAX 908-764-7303

CERTIFICATION OF ANALYSIS-EPA PROTOCOL

Date Shipped 07-16-1992
 certified per Protocol#1 Procedure 3.0.4-G1

Our Project 0716223

Your P.O. A-8434
 Top Pressure 2000psig

REFERENCE STD
 CYL. num

CRM/SRM. num 1005

STD conc. 250 ppm

MAKE/ model LAST cat.

ANAL prin.

MINOR comp. Nitric oxide 122ppm +/- 1%

TECO-108-20404 225-3/15/82-Chemluminescence

BALANCE Nitrogen o2 free

EXPIRES 1-15-1994

ANALYZER READINGS

Component

First Analysis

Second Analysis

Nitric Oxide

all values in ppm

Date: 07-08-1992 Item test array 122

Zero= 0 Ref. = 250 Test=122

Ref. = 250 Zero= 0 Test=122

Zero= 0 Test=122 Ref. = 250

Date: 07-15-1992 Item test array 122

Zero= 0 Ref. = 250 Test=122

Ref. = 250 Zero= 0 Test=122

Zero= 0 Test=122 Ref. = 250

ANALYST

Adela Sy

APPROVED BY

John O'Shea

CERTIFICATION OF ANALYSIS-EPA PROTOCOL

Date Shipped 12-07-1992

Certified per Protocol#1 Procedure 3.0.4-G1

Cylinder # ALM008187

MINOR

CERT.

CONC.

270ppm+-1%

Nitric Oxide

Our Project 0718209

Top Pressure 2000psi

REFERENCE STD

CRM/CRM

NUM

18080

CYL.

NUM

CLM979

STD

CONC.

244.4 ppm

MAKE/

model

cal.

Your P.O. #9560

GAS ANALYZER

LAST

prin.

ANAL

prin.

TECO-103-28404 228-11/15/92-Chromluminescence

EXPIRES 8-07-1994

BALANCE Nitrogen o2 free

ANALYZER READINGS

Component

Nitric Oxide

all values in ppm

First Analysis

Date: 11-30-1992 Mean test assay 278
Zero: 0 Ref. # 244.4 Test: 278
Ref. # 244.4 Zero: 0 Test: 278
Zero: 0 Test: 278

Second Analysis

Date: 12-07-1992 Mean test assay 277
Zero: 0 Ref. # 244.4 Test: 278
Ref. # 244.4 Zero: 0 Test: 278
Zero: 0 Test: 278 Ref. # 244.4

ANALYST

Adela Sy

APPROVED BY John O'Shea

JO

PHONE 908-764-7700 FAX 908-764-7303

CERTIFICATION OF ANALYSIS-EPA PROTOCOL

Date Shipped 08-24-1993
Certified per Protocol#1 Procedure 3.0.4-G1
Cylinder # ALM033324

MINOR
comp. CERT. Our Project 0721482

Nitric Oxide
505ppm +/- 1%
505ppm

CRM/CRM
NUM 1687

REFERENCE STD
CYL. NUM
AL19904

STD
CONC.
987.5 ppm

Top Pressure 2000psi
MAKE/ MODEL
GAS ANALYZER
LAST CAL.

Our P.O. 190835
TECO-109-28404 225-5/15/93-CHEMILUMINESCENCE

NOX

BALANCE Nitrogen O2 Free

ANALYZER READINGS

Component

First Analysis

Nitric Oxide

all values as ppm

Date: 08-14-1993
Zero 0 Ref. = 987.5
Ref. = 987.5 Zero 0
Zero 0 Test = 505 Ref. = 987.5

Second Analysis

Date: 08-24-1993
Zero 0 Ref. = 987.5
Ref. = 987.5 Zero 0
Zero 0 Test = 504 Ref. = 987.5

EXPIRES 12-24-1994 (acid rain)
6-24-1995 (general)

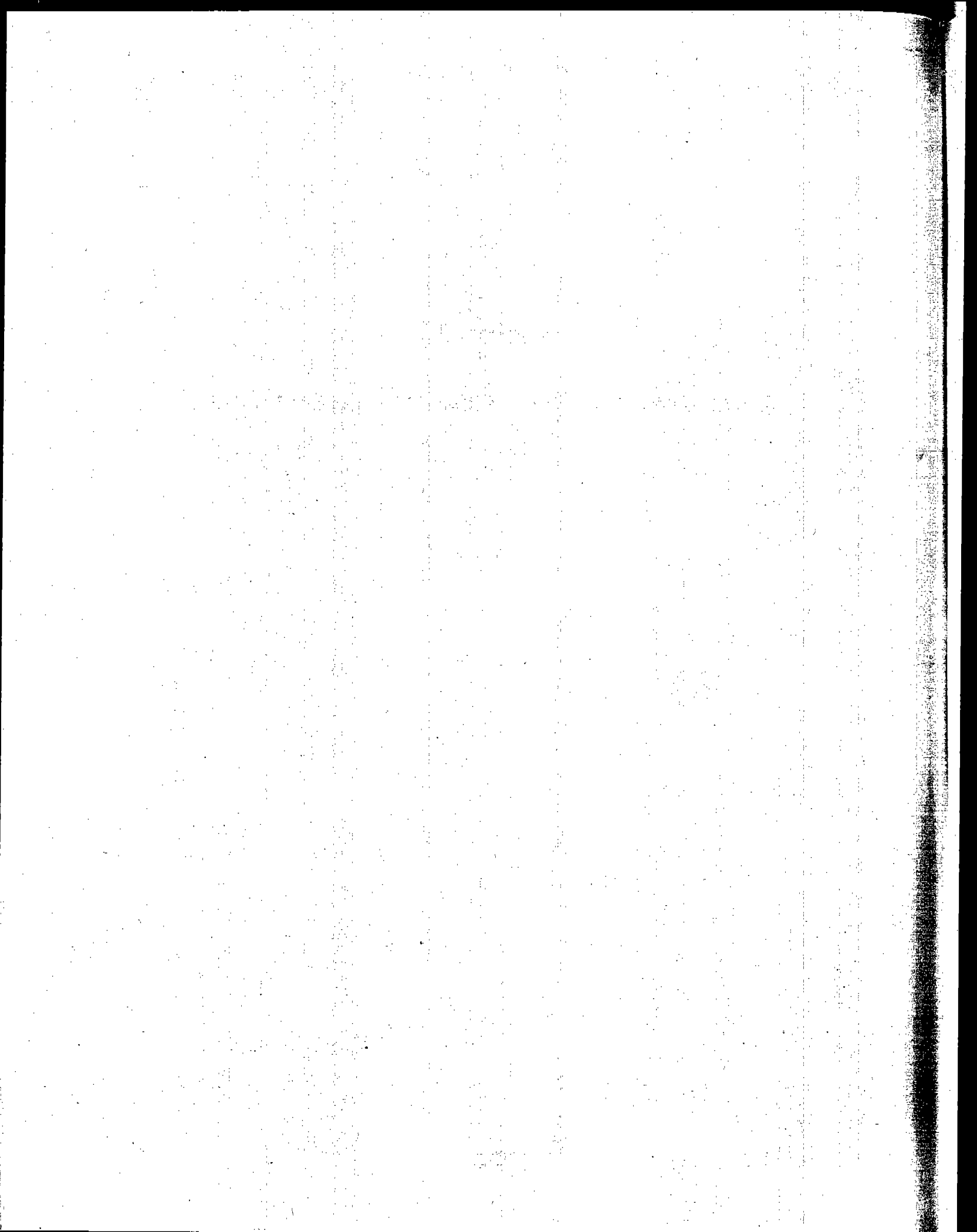
ANALYST

Adela By

APPROVED BY  John O'Shea

APPENDIX C

GAS CHROMATOGRAPH DATA AND CALIBRATION SHEETS



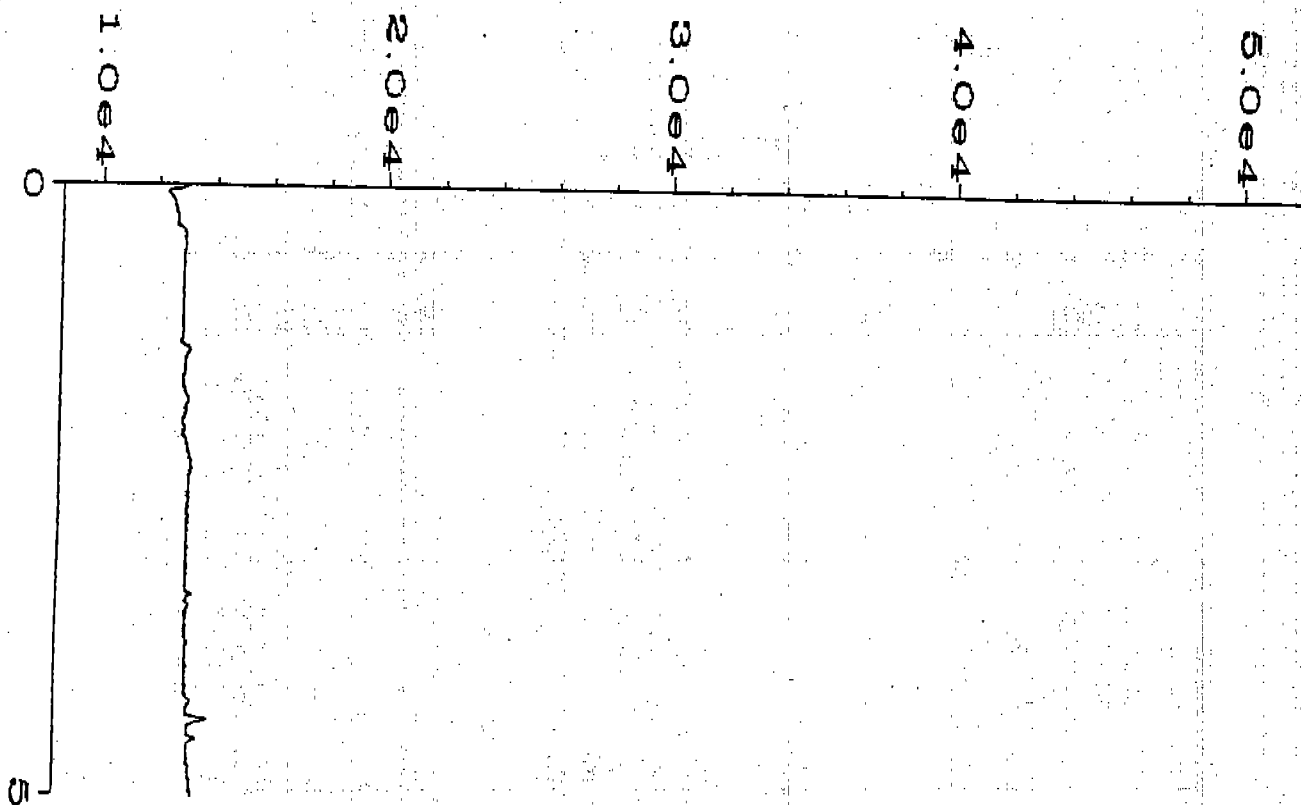
**BFI Chicopee
Engine #1 - Methane Emissions**

Date	Run #	Injection #	Methane (ppm)
12/14/93	1	1	2,020.9
12/14/93	1	2	2,040.4
12/14/93	1	3	2,073.5
AVERAGE			2,044.9
12/14/93	2	1	2,074.2
12/14/93	2	2	2,050.8
12/14/93	2	3	2,038.5
AVERAGE			2,054.5
12/14/93	3	1	1,993.0
12/14/93	3	2	2,005.7
12/14/93	3	3	1,985.0
AVERAGE			1,994.6

TOTAL AVERAGE 2,031.3

BFIC-M-1.WK1

run Methane
#1



Calibrated report not possible because no calibration table exists

Area Percent Report

File Name : C:\NPFICHE\1\DATA\NV-F0480.D

Detector

Instrument : FID/FPD

File Name

Time Base Code

Printed on : 14 Dec 93 06:18 PM

Print Created on: 14 Dec 93 06:28 PM

Page Number : 1

Vial Number :

Injection Number :

Sequence Line :

Instrument Method: MMT5.MTH

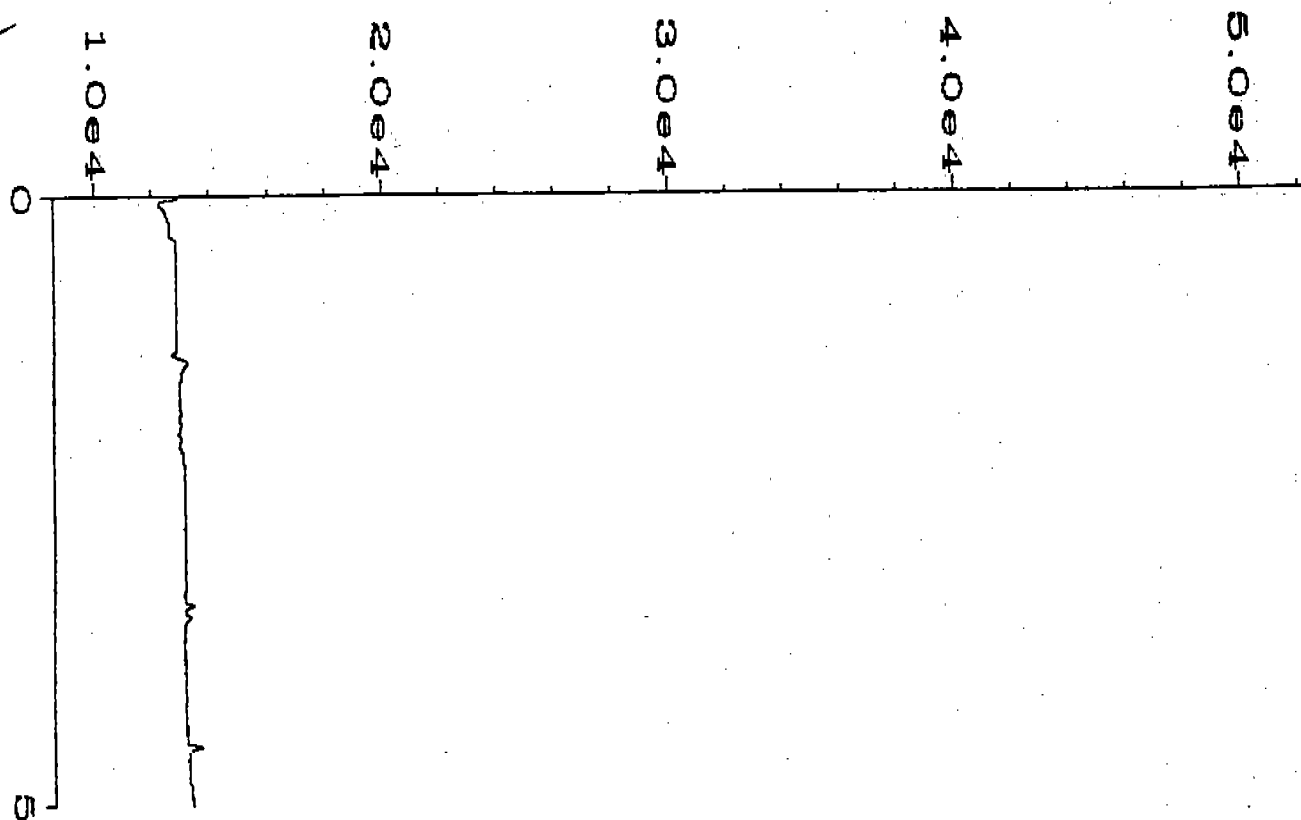
Analysis Method : MMT5.MTH

1 in C:\NPFICHE\1\DATA\NV-F0480.D

PK#	Ret Time	Area	Height	Type	Width	Area %
-----	----------	------	--------	------	-------	--------

Total area = 0

4000000000
#2



Calibrated report not possible because no calibration table exists

=====
Area Percent Report
=====

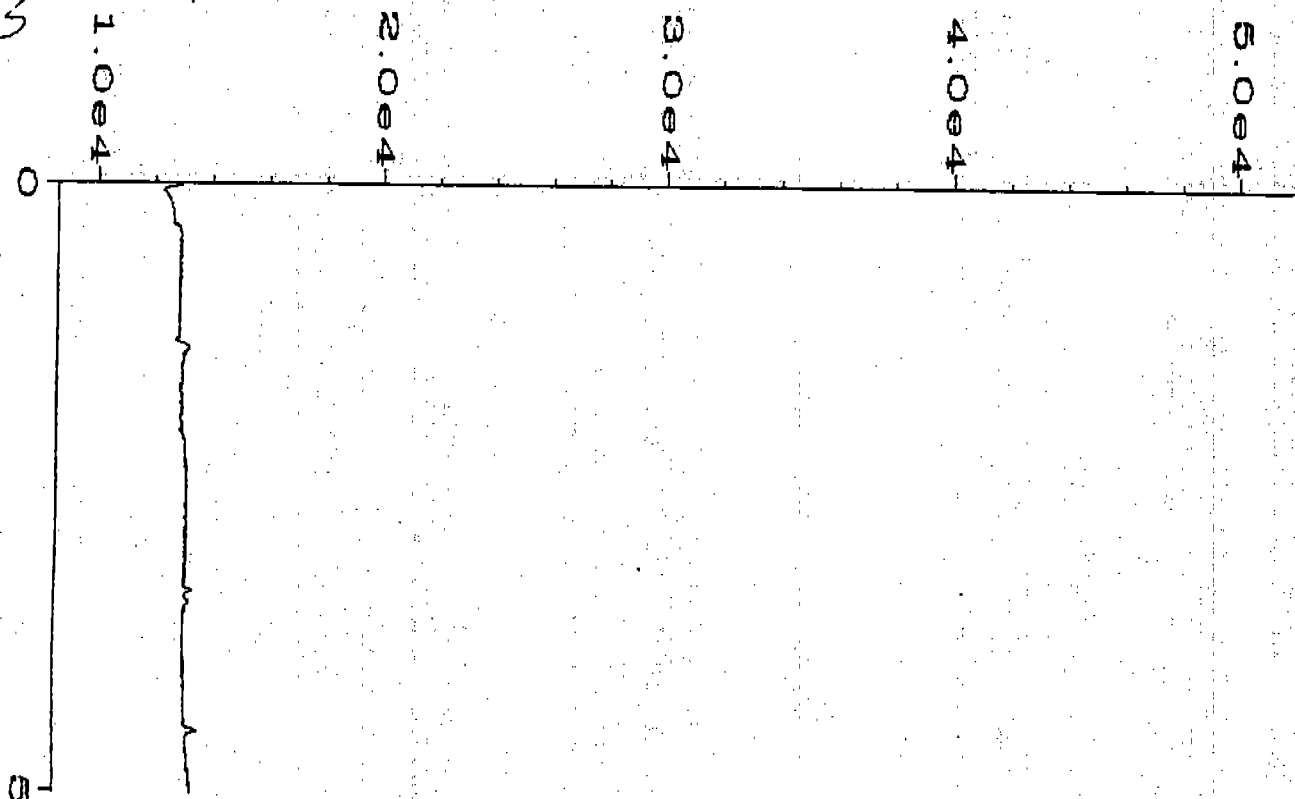
File Name	: C:\MSDCHEM\1\DATA\NV-F0481.D	Page Number	: 1
Detector	:	Vial Number	:
Instrument	: FID/FPD	Injection Number	:
File Name	:	Sequence Line	:
Time Bar Code	:	Instrument Method	: MMT5.MTH
Printed on	: 14 Dec 93 08:29 PM	Analysis Method	: MMT5.MTH
Not created on	: 14 Dec 93 08:35 PM		

1 in C:\MSDCHEM\1\DATA\NV-F0481.D

Peak	Ret Time	Area	Height	Type	Width	Area %
1		area = 0				

=====

in Methane
#3



brated report not possible because no calibration table exists

Area Percent Report

File Name : C:\HPCHEM\1\DATA\NV-F0482.D

ator :

Page Number : 1

ument : FID/FPD

Vial Number :

le Name :

Injection Number :

Time Bar Code:

Sequence Line :

red on : 14 Dec 93 06:37 PM

Instrument Method: MMT5.MTH

rt Created on: 14 Dec 93 06:43 PM

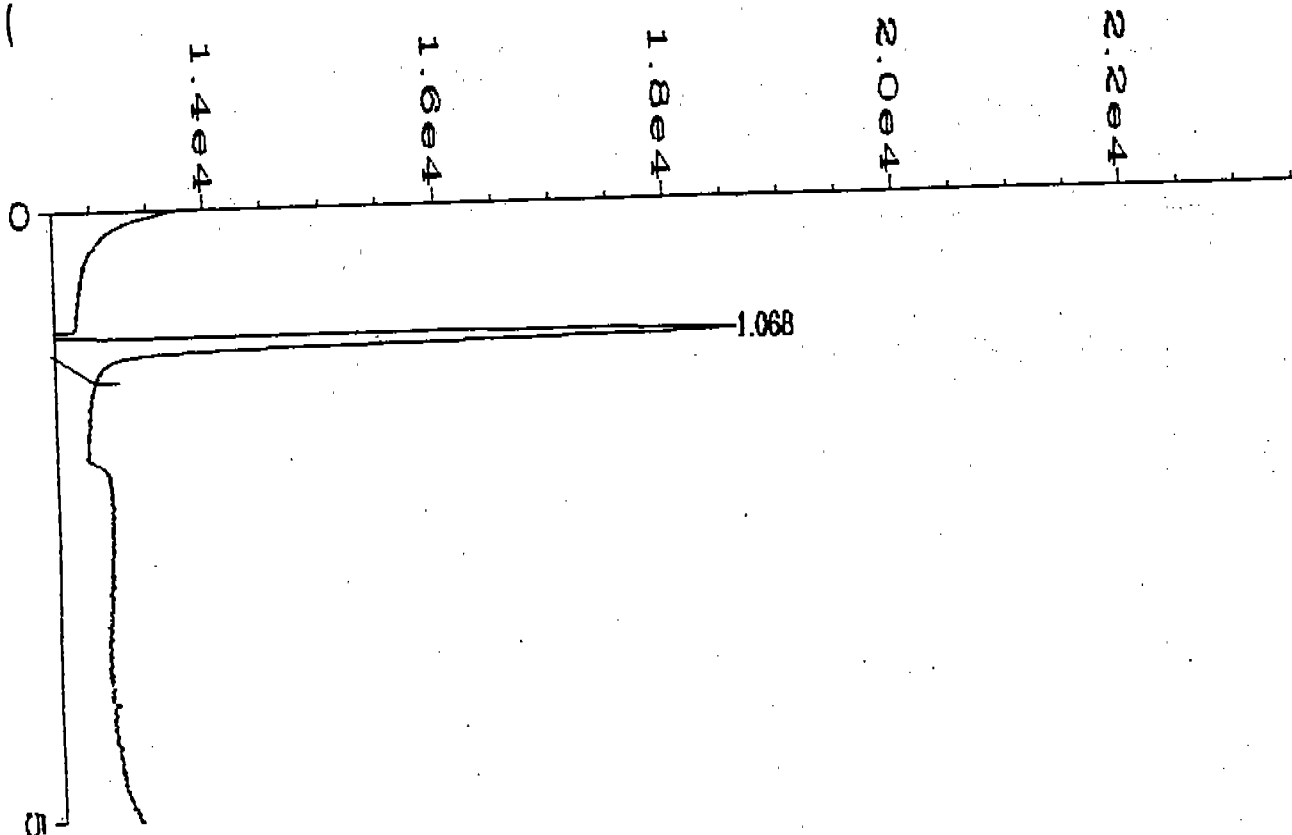
Analysis Method : MMT5.MTH

1 in C:\HPCHEM\1\DATA\NV-F0482.D

Plk#	Ret Time	Area	Height	Type	Width	Area %
------	----------	------	--------	------	-------	--------

1 area = 0

1 ppm Methane
#1



External Standard Report

File Name : C:\NPPCHEM\1\DATA\NV-F0484.D
 Detector :
 Instrument : FID/FPD
 File Name :
 Time Bar Code:
 Printed on : 14 Dec 93 06:58 PM
 Report Created on: 14 Dec 93 07:06 PM
 Recalibrated on : 14 Dec 93 07:05 PM
 Multiplier : 1

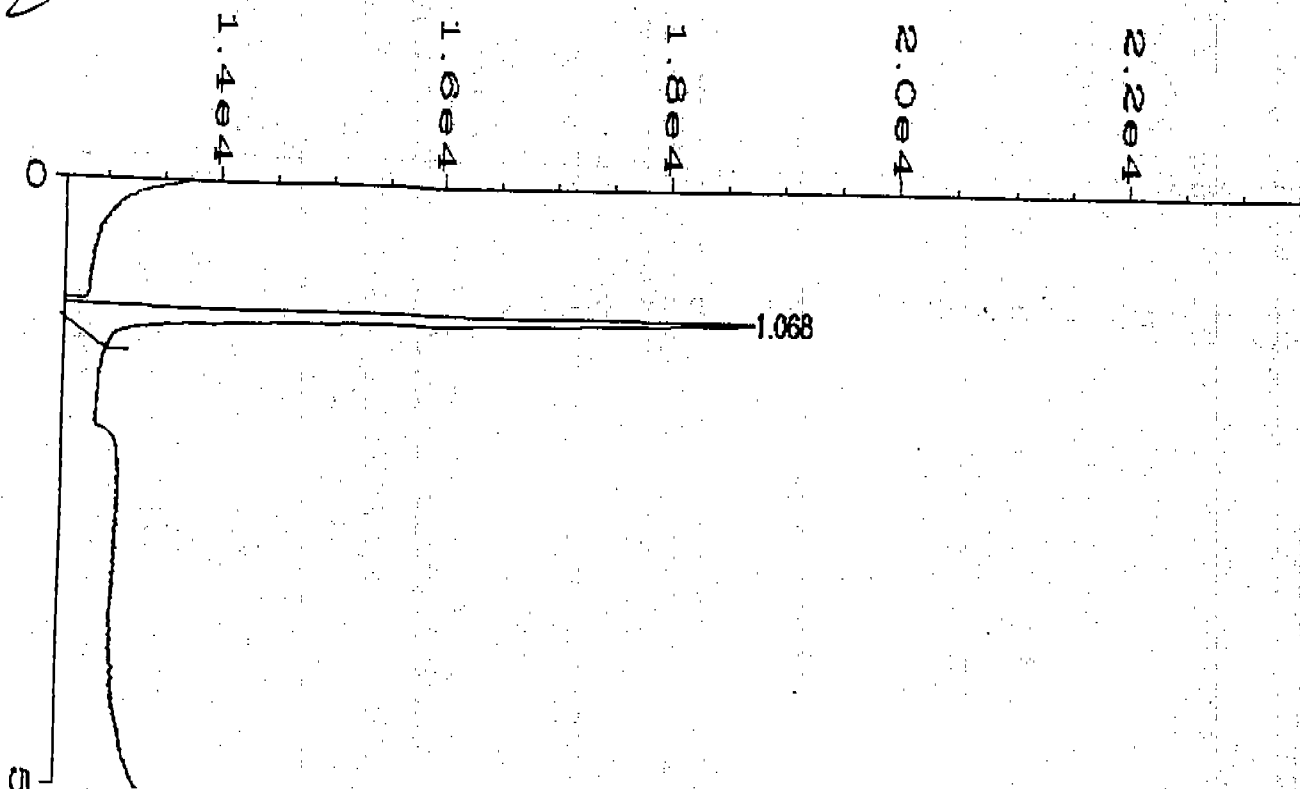
Page Number : 1
 Vial Number :
 Injection Number :
 Sequence Line :
 Instrument Method: MMT5.MTH
 Analysis Method : MMT5.MTH
 Sample Amount : 0
 ISTD Amount :

1 in C:\NPPCHEM\1\DATA\NV-F0484.D

Time	Area	Type	Width	Ref#	PPM	Name
1.068	36026	BB	0.094	1-R	48.900	METHANE

Time Reference Peak	Expected RT	Actual RT	Difference
1	1.068	1.068	0.0%

1 ppm Methane
#2



External Standard Report

File Name : C:\HPCHEM\1\DATA\NV-F0485.D
 ator :
 rument : FID/FPS
 le Name :
 Time Bar Code:
 ired ch : 14 Dec 93 07:06 PM
 rt Created on: 14 Dec 93 07:14 PM
 Rec'd on : 14 Dec 93 07:12 PM
 plier : 1

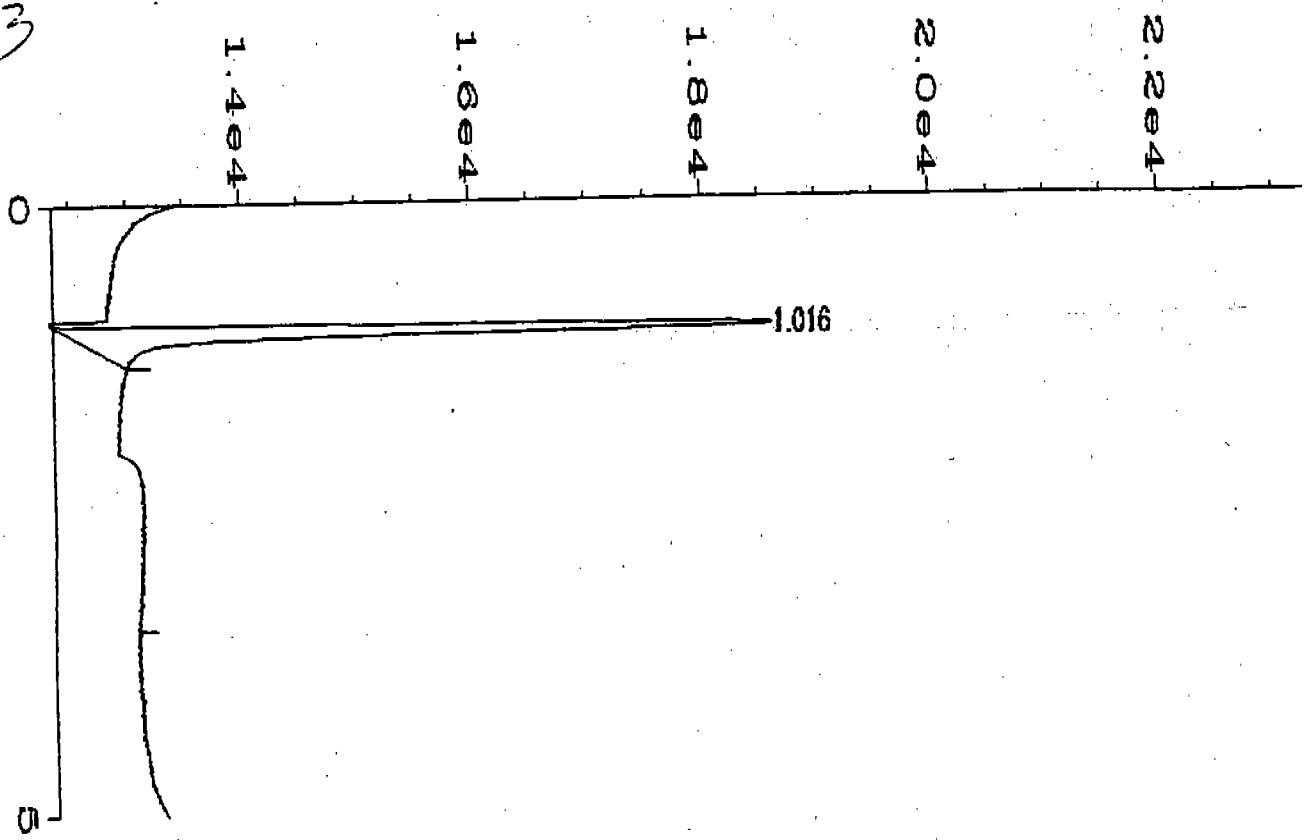
Page Number : 1
 Vial Number :
 Injection Number :
 Sequence Line :
 Instrument Method: MMT5.MTH
 Analysis Method : MMT5.MTH
 Sample Amount : 0
 ISTD Amount :

1 in C:\HPCHEM\1\DATA\NV-F0485.D

Time	Area	Type	Width	Ref#	PPM	Name
1.068	35291	BB	0.091	1-R	48.396	METHANE

Time Reference Peak	Expected RT	Actual RT	Difference
1	1.068	1.068	0.0%

ppm Methane
#3



External Standard Report

File Name : C:\NFCHEM\1\DATA\NV-F0486.D
 Instrument : FID/FPD
 Sample Name :
 Time Bar Code:
 Created on : 14 Dec 93 07:15 PM
 Report Created on: 14 Dec 93 07:24 PM
 Recalib on : 14 Dec 93 07:24 PM
 Multiplier : 1

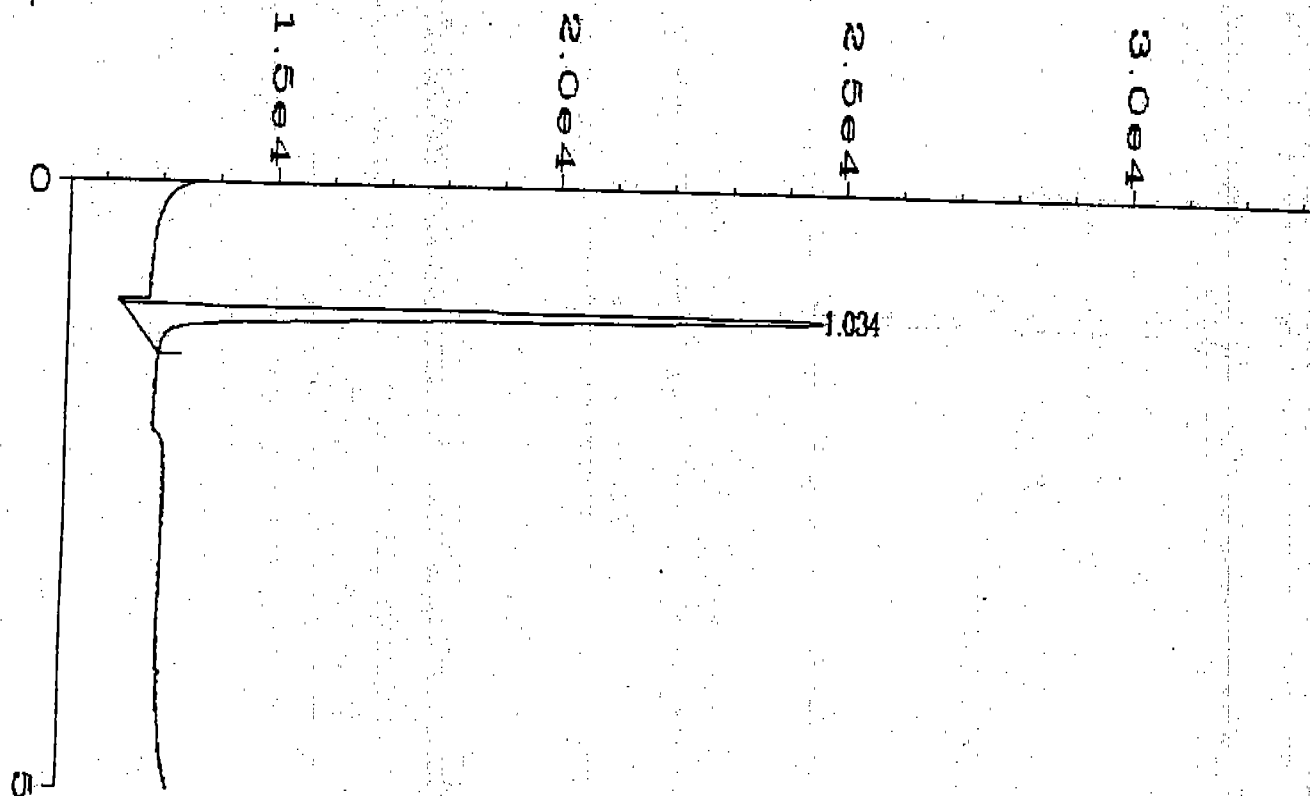
Page Number : 1
 Vial Number :
 Injection Number :
 Sequence Line :
 Instrument Method: MMT5.MTH
 Analysis Method : MMT5.MTH
 Sample Amount : 0
 ISTD Amount :

1 in C:\NFCHEM\1\DATA\NV-F0486.D

Time	Area	Type	Width	Ref#	PPM	Name
1.016	35184	BB	0.090	1-R	48.464	METHANE

Time Reference Peak	Expected RT	Actual RT	Difference
1	1.027	1.016	-1.0%

C ppm Methane
#1



External Standard Report

File Name : C:\HFCHEN\1\DATA\NV-F0487.D
 Instrument : FID/FPS
 Time Bar Code:
 Date on : 14 Dec 93 07:25 PM
 Port Created on: 14 Dec 93 07:33 PM
 Recalib on: 14 Dec 93 07:32 PM
 Multiplier : 1

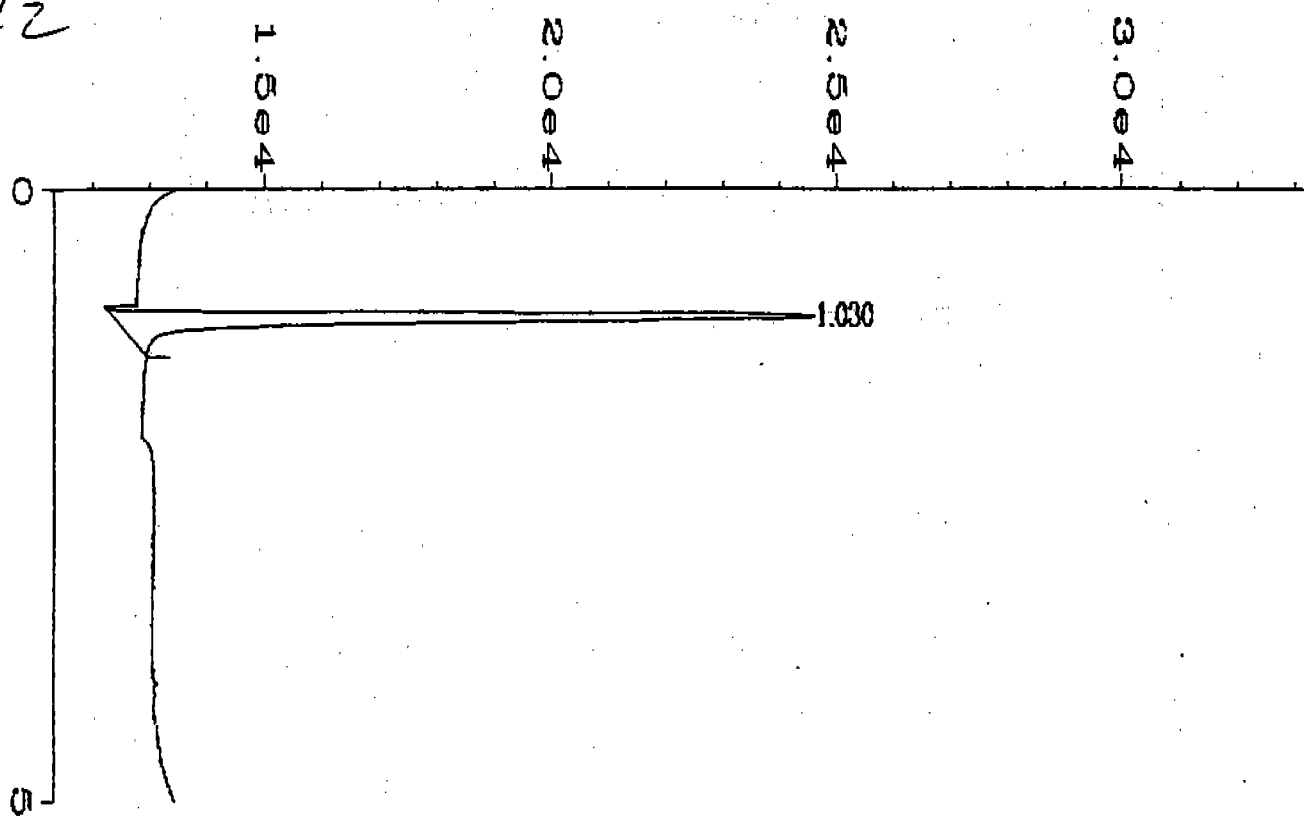
Page Number : 1
 Vial Number :
 Injection Number :
 Sequence Line :
 Instrument Method: MMT5.MTH
 Analysis Method : MMT5.MTH
 Sample Amount : 0
 ISTD Amount :

1 in C:\HFCHEN\1\DATA\NV-F0487.D

Time	Area	Type	Width	Ref#	PPM	Name
1.034	71025	BB	0.092	1-R	102.000	METHANE

Time Reference Peak	Expected RT	Actual RT	Difference
1	1.027	1.034	0.7%

2 ppm Methane
y#2



External Standard Report

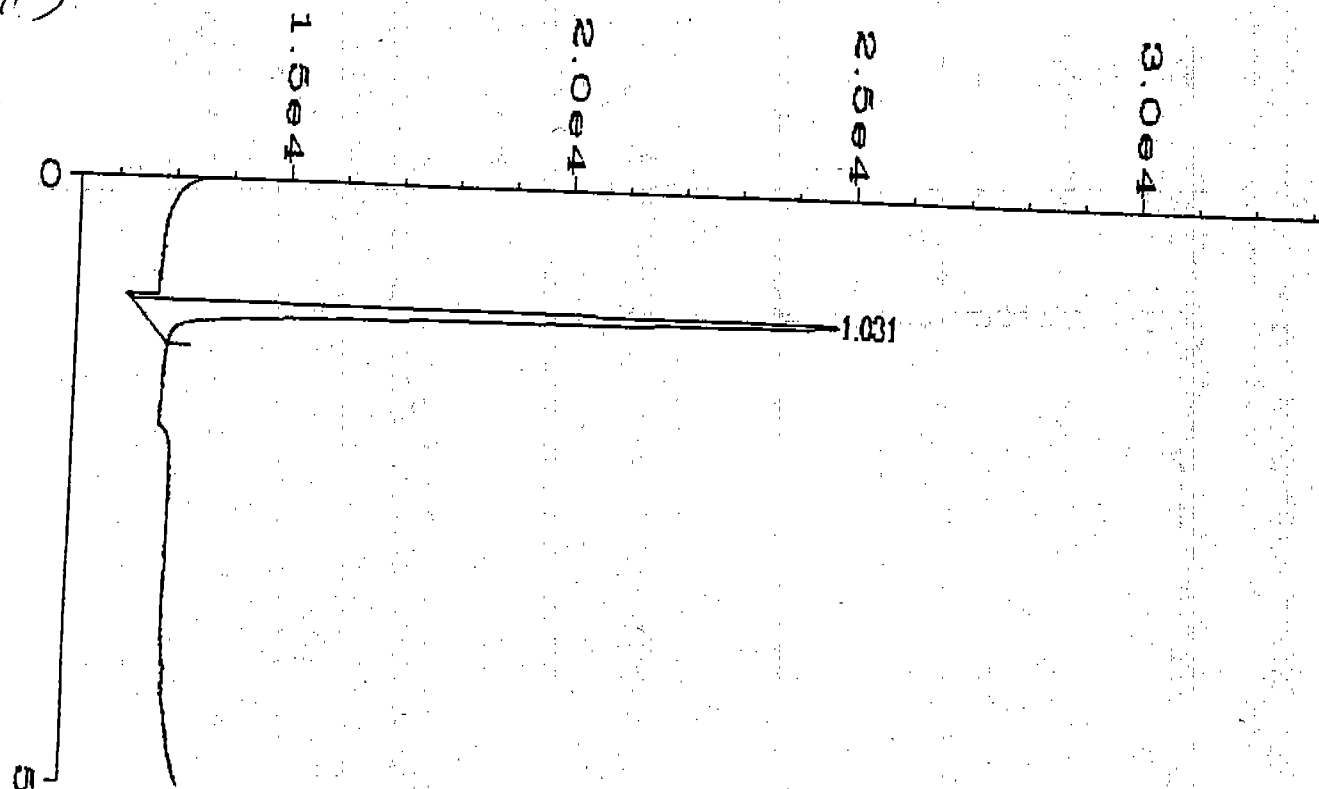
File Name : C:\HPCHEM\1\DATA\NV-F0489.D
ator :
rument : FID/FPD
le Name :
Time Bar Code:
ired on : 14 Dec 93 07:42 PM
rt Created on: 14 Dec 93 07:49 PM
Recalib on : 14 Dec 93 07:48 PM
plier : 1
Page Number : 1
Vial Number :
Injection Number :
Sequence Line :
Instrument Method: MMT5.MTH
Analysis Method : MMT5.MTH
Sample Amount : 0
ISTD Amount :

1 in C:\HPCHEM\1\DATA\NV-F0489.D

Time	Area	Type	Width	Ref#	PPM	Name
1.030	70338	BB	0.092	1-R	101.482	METHANE

Time Reference Peak	Expected RT	Actual RT	Difference
1	1.038	1.030	-0.7%

ppm Methane
#3



External Standard Report

File Name : C:\HPCHEM\1\DATA\NV-F0491.D
 ator :
 rument : FID/FPD
 ie Name :
 Time Bar Code:
 ired on : 14 Dec 93 07:59 PM
 rt Created on: 14 Dec 93 08:05 PM
 Rata/b on : 14 Dec 93 08:05 PM
 plier : 1

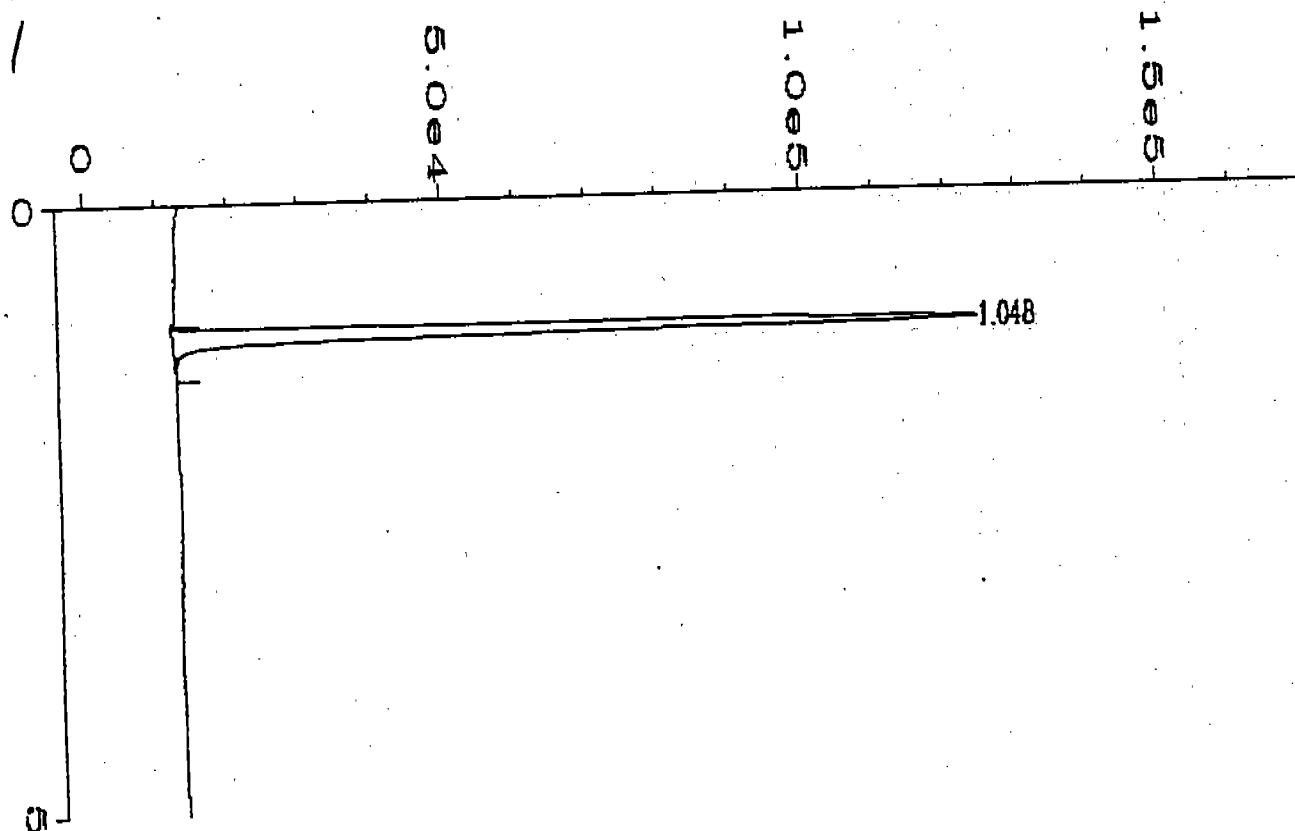
Page Number : 1
 Vial Number :
 Injection Number :
 Sequence Line :
 Instrument Method: FID5.MTH
 Analysis Method : FID5.MTH
 Sample Amount : 0
 ISTD Amount :

1 in C:\HPCHEM\1\DATA\NV-F0491.D

Time	Area	Type	Width	Ref#	PPM	Name
1.031	70458	BB	0.090	1-R	101.774	METHANE

Time Reference Peak	Expected RT	Actual RT	Difference
1	1.036	1.031	-0.5%

4 ppm Methane
#1



External Standard Report

File Name : C:\HPCHEM\1\DATA\NV-F0492.D
 Detector : FID/FPD
 Sample Name :
 Time Bar Code:
 Printed on : 14 Dec 93 08:07 PM
 Report Created on: 14 Dec 93 08:14 PM
 Recalib on : 14 Dec 93 08:13 PM
 Multiplier : 1

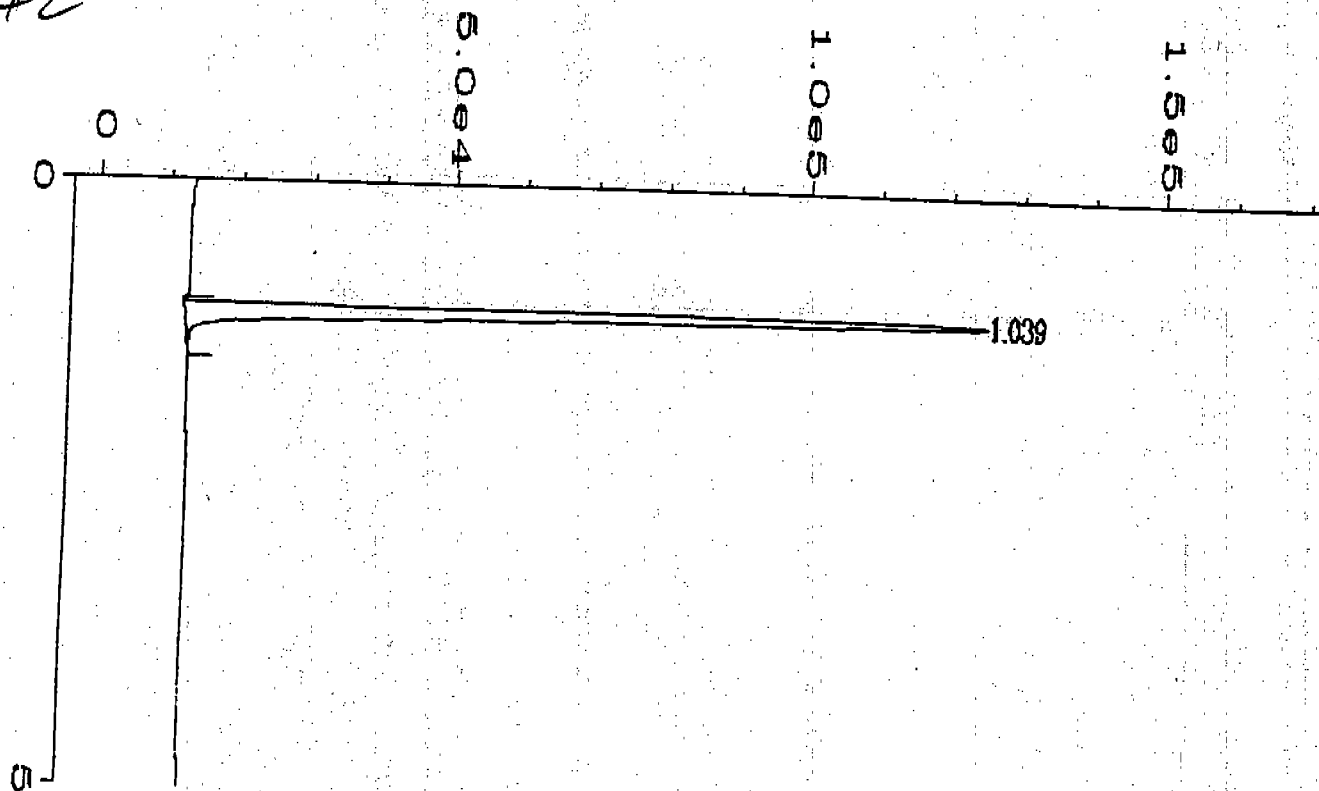
Page Number : 1
 Vial Number :
 Injection Number :
 Sequence Line :
 Instrument Method: HMT5.MTH
 Analysis Method : HMT5.MTH
 Sample Amount : 0
 ISTD Amount :

1 in C:\HPCHEM\1\DATA\NV-F0492.D

Time	Area	Type	Width	Ref#	PPM	Name
1.048	582098	BB	0.084	1-R	983.790	METHANE

Time Reference Peak	Expected RT	Actual RT	Difference
1	1.036	1.048	1.2%

1 ppm Methane
j#2



External Standard Report

File Name : C:\HPCHEM\1\DATA\NV-F0493.D
 Detector :
 Instrument : FID/FPD
 Sample Name :
 Time Bar Code :
 Acquired on : 14 Dec 93 08:16 PM
 Report Created on : 14 Dec 93 08:22 PM
 Recalib on : 14 Dec 93 08:21 PM
 Multiplier : 1

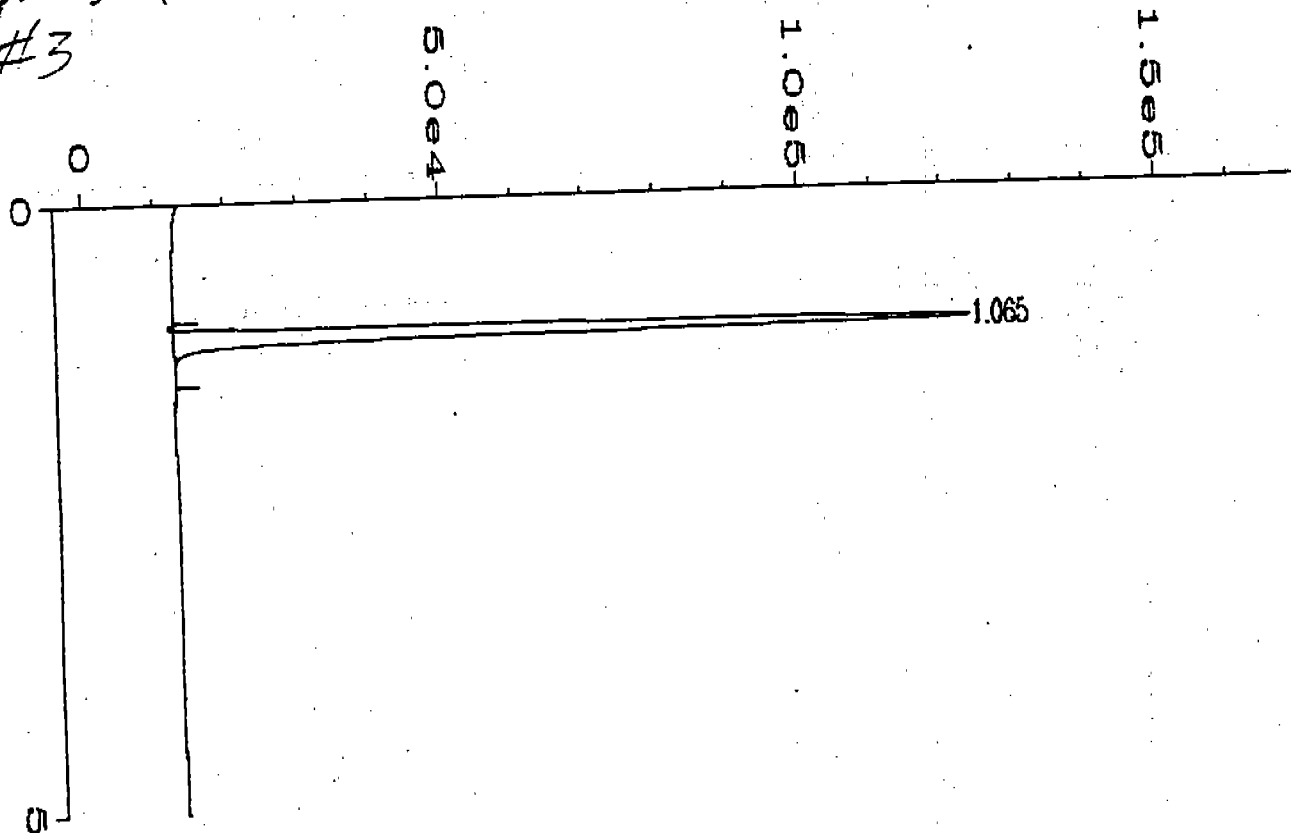
Page Number : 1
 Vial Number :
 Injection Number :
 Sequence Line :
 Instrument Method: MMT5.MTH
 Analysis Method : MMT5.MTH
 Sample Amount : 0
 ISTD Amount :

1. In C:\HPCHEM\1\DATA\NV-F0493.D

Time	Area	Type	Width	Ref#	PPM	Name
1.039	580609	BB	0.083	1-R	982,508	METHANE

Time Reference Peak	Expected RT	Actual RT	Difference
1	1.037	1.039	0.2%

34 ppm Methane
Inj #3



External Standard Report

File Name : C:\HPCHEM\1\DATA\NV-F0494.D
 Detector :
 Instrument : FID/FPD
 File Name :
 Time Bar Code:
 Acquired on : 14 Dec 93 08:24 PM
 Report Created on: 14 Dec 93 08:32 PM
 Last Recalib on : 14 Dec 93 08:31 PM
 Multiplier : 1

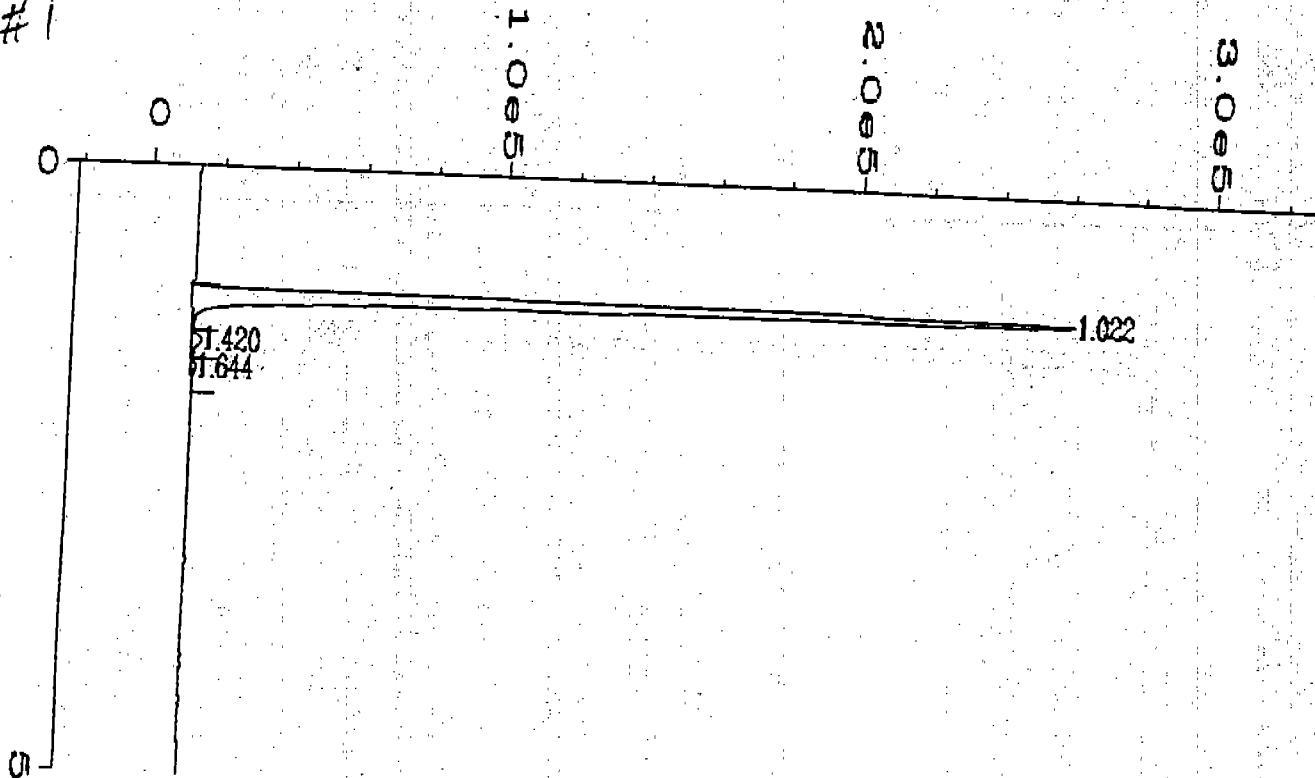
Page Number : 1
 Vial Number :
 Injection Number :
 Sequence Line :
 Instrument Method: MMT5.MTH
 Analysis Method : MMT5.MTH
 Sample Amount : 0
 ISTD Amount :

1 in C:\HPCHEM\1\DATA\NV-F0494.D

Time	Area	Type	Width	Ref#	PPM	Name
1.065	577506	BE	0.085	1-R	979.363	METHANE

Time Reference Peak	Expected RT	Actual RT	Difference
1	1.054	1.065	1.1%

ack #1
in #1
j #1



External Standard Report

File Name : C:\HPCHEM\1\DATA\NV-F0495.D
 ator :
 Instrument : FID/FID
 File Name :
 Time Bar Code :
 Printed on : 14 Dec 93 08:34 PM
 Port Created on : 14 Dec 93 08:42 PM
 Recalib on : 14 Dec 93 08:31 PM
 plier : 1

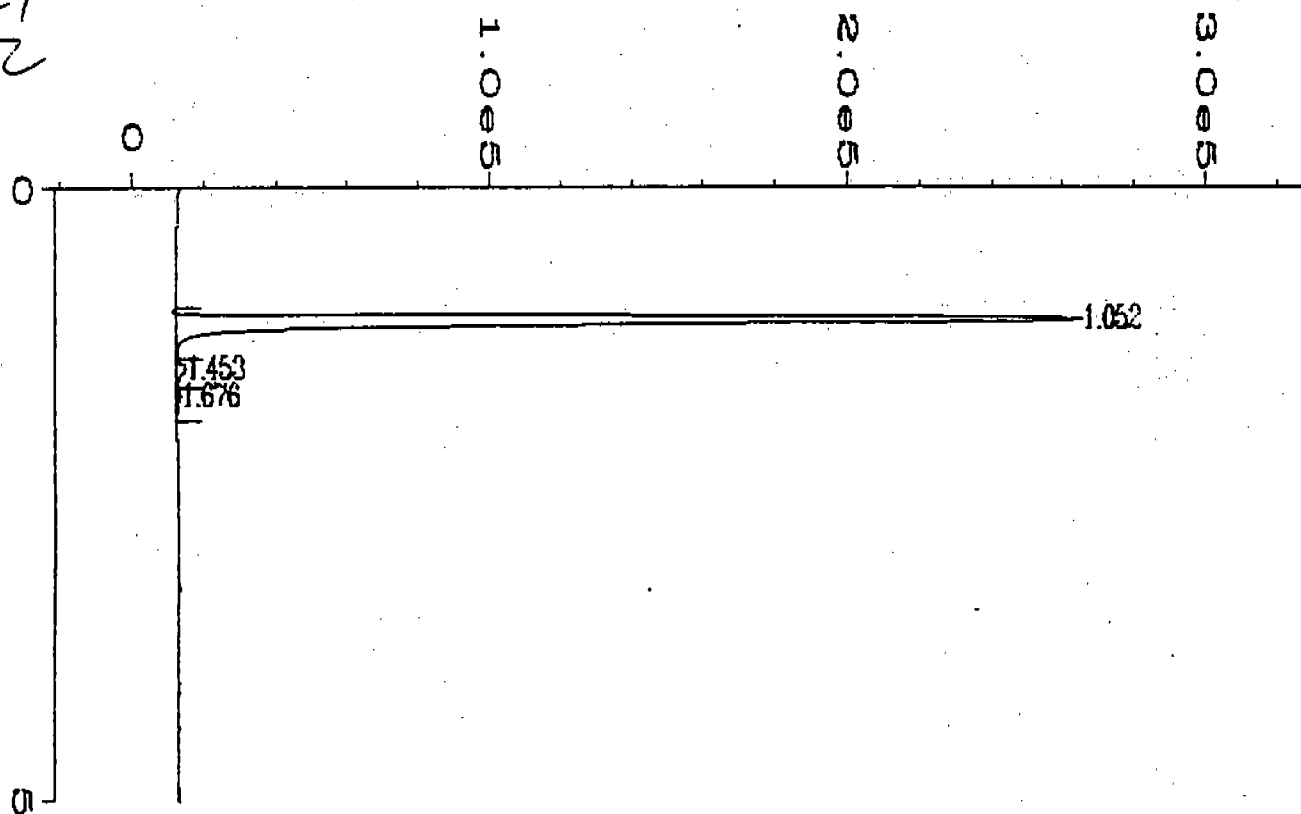
Page Number : 1
 Vial Number :
 Injection Number :
 Sequence Line :
 Instrument Method: MMT5.MTH
 Analysis Method : MMT5.MTH
 Sample Amount : 0
 ISTD Amount :

1 in C:\HPCHEM\1\DATA\NV-F0495.D

Time	Area	Type	Width	Ref#	PPM	Name
1.022	1181868	BV	0.076	1-R	2020.879	METHANE

Time Reference Peak	Expected RT	Actual RT	Difference
1	1.030	1.022	-0.8%

CK #1
#1
#2



External Standard Report

File Name : C:\HPCHEM\1\DATA\NV-F0496.D

Instrument : FID/FPD

Sample Name :

Time Bar Code:

Printed on : 14 Dec 93 08:43 PM

Report Created on: 14 Dec 93 08:49 PM

Recalib on : 14 Dec 93 08:31 PM

Multiplier : 1

Page Number : 1

Vial Number :

Injection Number :

Sequence Line :

Instrument Method: MMT5.MTH

Analysis Method : MMT5.MTH

Sample Amount : 0

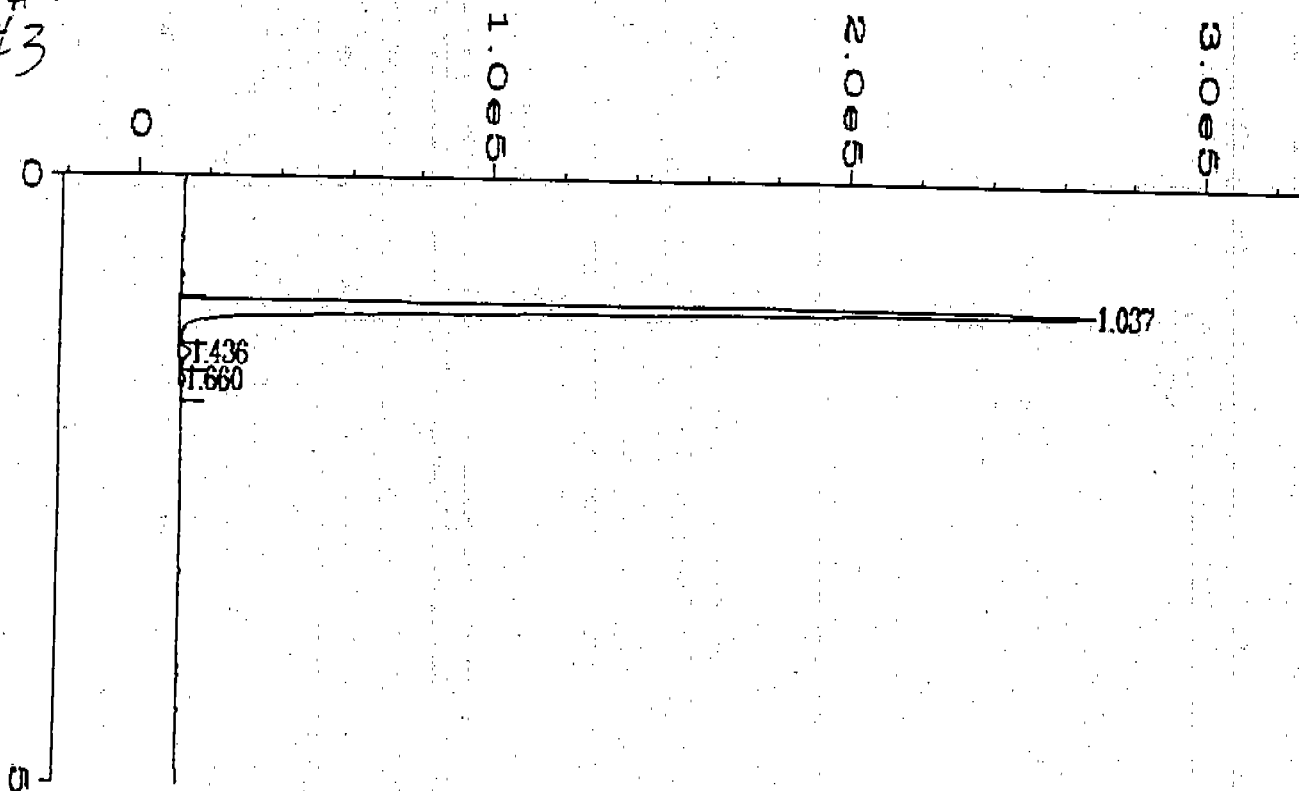
ISTD Amount :

1 in C:\HPCHEM\1\DATA\NV-F0496.D

Time	Area	Type	Width	Ref#	PPM	Name
1.052	1193205	BV	0.076	1-R	2040.417	METHANE

Time Reference Peak	Expected RT	Actual RT	Difference
1	1.030	1.052	2.1%

ack #1
n #1
i #3



External Standard Report

File Name : C:\HPCHEM\1\DATA\NV-F0497.D
 Instrument : FID/FPD
 Sample Name :
 Time Bar Code:
 Printed on : 14 Dec 93 08:52 PM
 Report Created on: 14 Dec 93 08:58 PM
 Recalibrated on : 14 Dec 93 08:31 PM
 Injection : 1

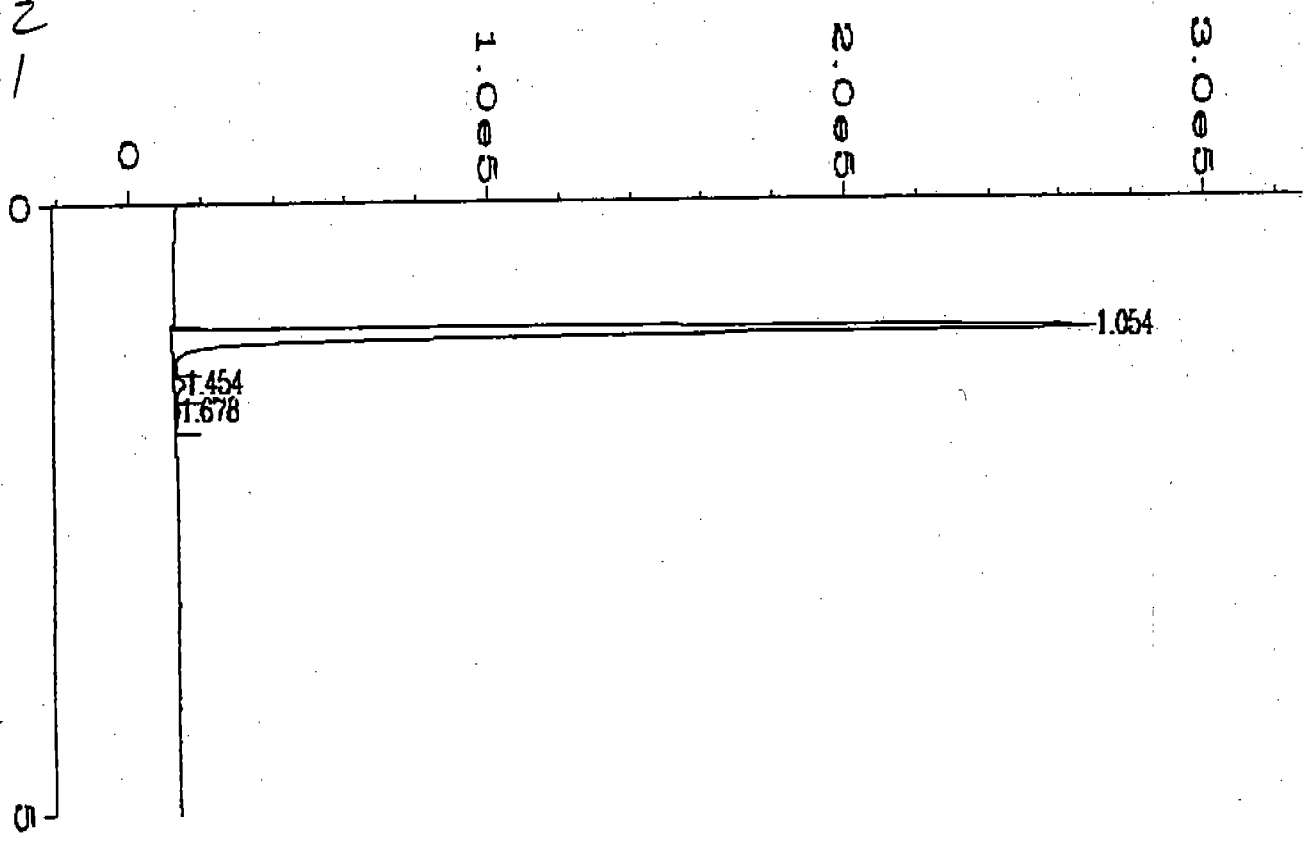
Page Number :
 Vial Number :
 Injection Number :
 Sequence Line :
 Instrument Method: MMTE.MTH
 Analysis Method : MMTE.MTH
 Sample Amount : 0
 ISTD Amount :

1 in. C:\HPCHEM\1\DATA\NV-F0497.D

Time	Area	Type	Width	Ref#	PPM	Name
1.037	1212390	BV	0.076	1-R	2073.479	METHANE

Time Reference Peak	Expected RT	Actual RT	Difference
1	1.030	1.037	0.7%

ck #1
 #2
 y #1



=====
 External Standard Report
 =====

File Name : C:\HPCHEM\1\DATA\NV-F0498.D
 Factor :
 Instrument : FID/FPD
 Sample Name :
 Time Bar Code :
 Acquired on : 14 Dec 93 09:00 PM
 Report Created on: 14 Dec 93 09:06 PM
 Recalibrated on : 14 Dec 93 08:31 PM
 Multiplier : 1

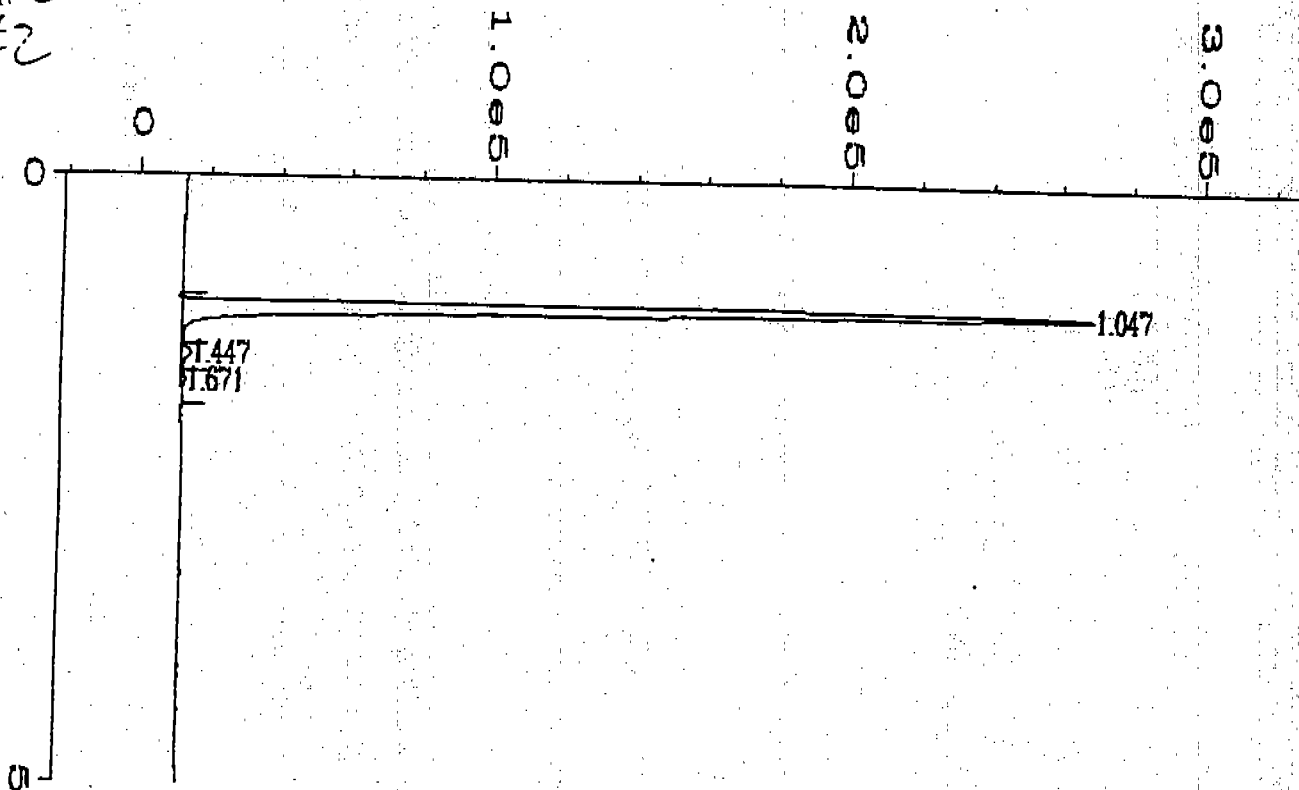
Page Number : 1
 Vial Number :
 Injection Number :
 Sequence Line :
 Instrument Method: MMT5.MTH
 Analysis Method : MMT5.MTH
 Sample Amount : 0
 ISTD Amount :

1 in C:\HPCHEM\1\DATA\NV-F0498.D

Time	Area	Type	Width	Ref#	PPM	Name
1.054	1212805	BV	0.076	1-R	2074.195	METHANE

Time Reference Peak	Expected RT	Actual RT	Difference
1	1.030	1.054	2.3%

ck #1
#2
#2



External Standard Report

File Name : C:\HPCHEM\1\DATA\NV-F0499.D
 ator :
 rument : FID/FPD
 le Name :
 Time Bar Code:
 ured on : 14 Dec 93 09:09 PM
 rt Created on: 14 Dec 93 09:14 PM
 ocalib on : 14 Dec 93 08:31 PM
 plier : 1

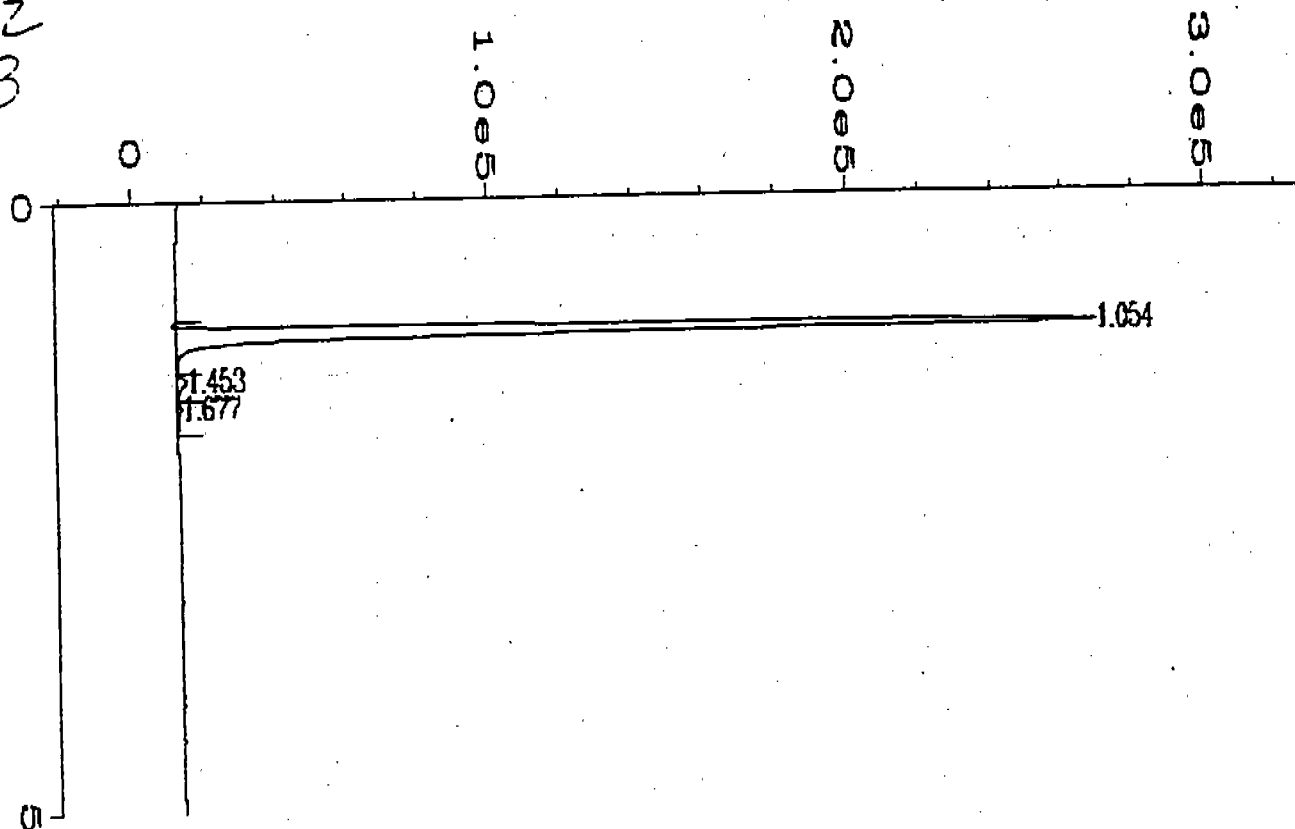
Page Number : 1
 Vial Number :
 Injection Number :
 Sequence Line :
 Instrument Method: MMT5.MTH
 Analysis Method : MMT5.MTH
 Sample Amount : 0
 ISTD Amount :

1 in C:\HPCHEM\1\DATA\NV-F0499.D

Time	Area	Type	Width	Ref#	PPM	Name
1.047	1199243	BV	0.075	1-R	2050.823	METHANE

Time Reference Peak	Expected RT	Actual RT	Difference
1	1.030	1.047	1.7%

K #1
#2
#3



External Standard Report

File Name : C:\HPCHEM\1\DATA\NV-F0501.D
 Detector :
 Instrument : PID/FID
 Sample Name :
 Time Bar Code:
 Acquired on : 14 Dec 93 09:17 PM
 Report Created on: 14 Dec 93 09:23 PM
 Last Recalib on : 14 Dec 93 08:31 PM
 Multiplier : 1

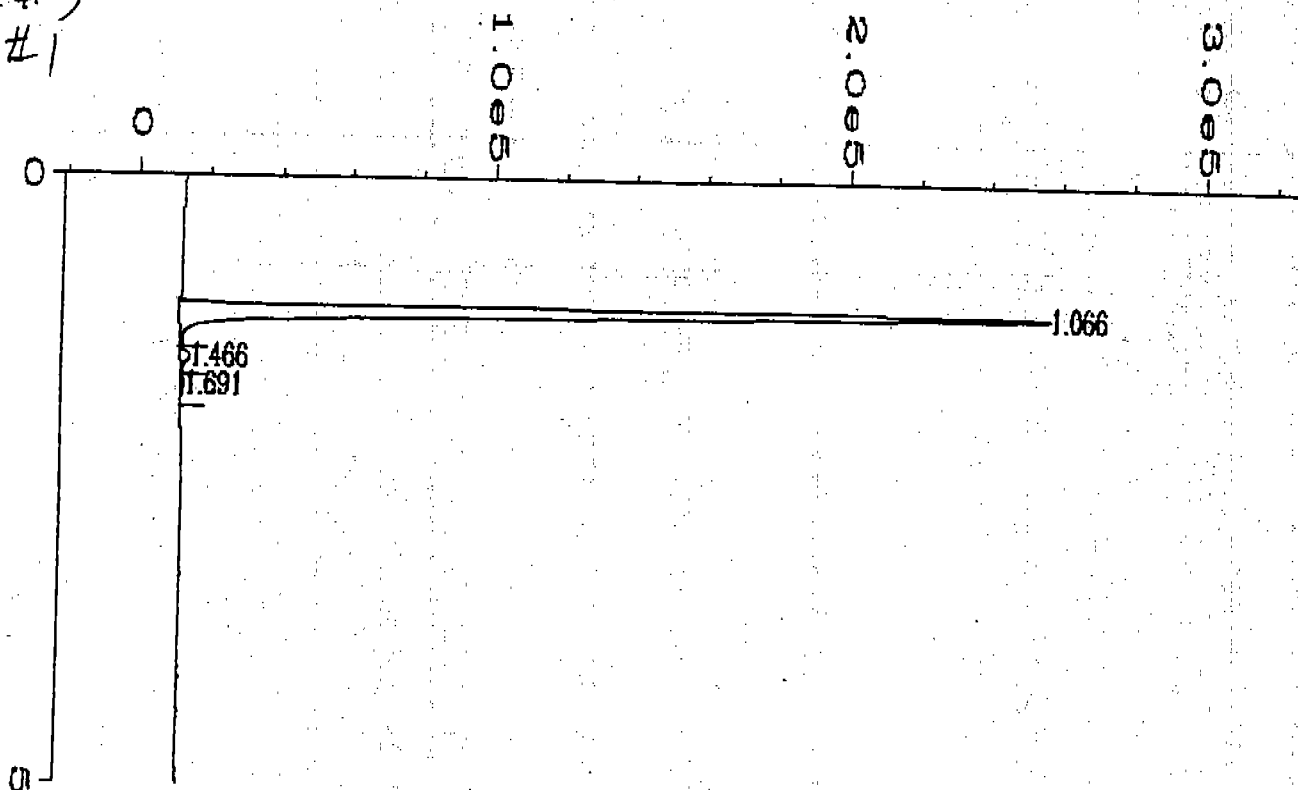
Page Number : 1
 Vial Number :
 Injection Number :
 Sequence Line :
 Instrument Method: MMT5.MTH
 Analysis Method : MMT5.MTH
 Sample Amount : 0
 ISTD Amount :

1 in C:\HPCHEM\1\DATA\NV-F0501.D

Time	Area	Type	Width	Ref#	PPM	Name
1.054	1192089	EV	0.075	1-R	2038.495	METHANE

Time Reference Peak	Expected RT	Actual RT	Difference
1	1.030	1.054	2.3%

ack #1
in #3
nj #1



External Standard Report

File Name : C:\HPCHEM\1\DATA\NV-F0502.D
 ator :
 rument : PID/FPD
 le Name :
 Time Bar Code:
 ired on : 14 Dec 93 09:26 PM
 nt Created on: 14 Dec 93 09:32 PM
 Retalib on : 14 Dec 93 08:31 PM
 iolier : 1

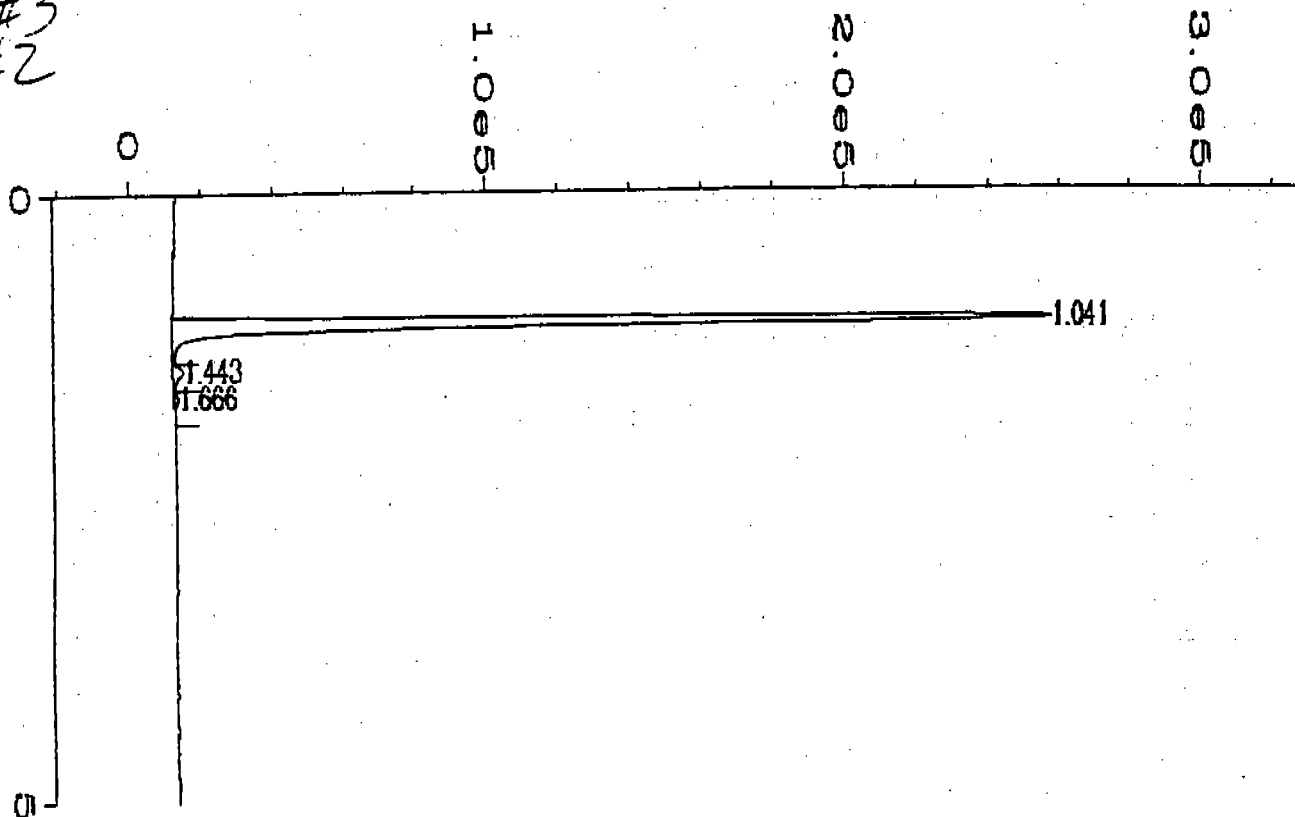
Page Number : 1
 Vial Number :
 Injection Number :
 Sequence Line :
 Instrument Method: MMTS.MTH
 Analysis Method : MMTS.MTH
 Sample Amount : 0
 ISTD Amount :

1 in C:\HPCHEM\1\DATA\NV-F0502.D

Time	Area	Type	Width	Ref#	FPM	Name
1.066	1165685	BV	0.077	1-R	1992.991	METHANE

Time Reference Peak	Expected RT	Actual RT	Difference
1	1.060	1.066	0.6%

ack #1
n #3
y #2



External Standard Report

File Name : D:\HPLCHEM\DATA\NV-F0503.D
 ator :
 rument : FID/SPD
 ic Name :
 Time Bar Code :
 ired on : 14 Dec 93 09:34 PM
 rt Created on : 14 Dec 93 09:40 PM
 Rec'd on : 14 Dec 93 08:31 PM
 plier : 1

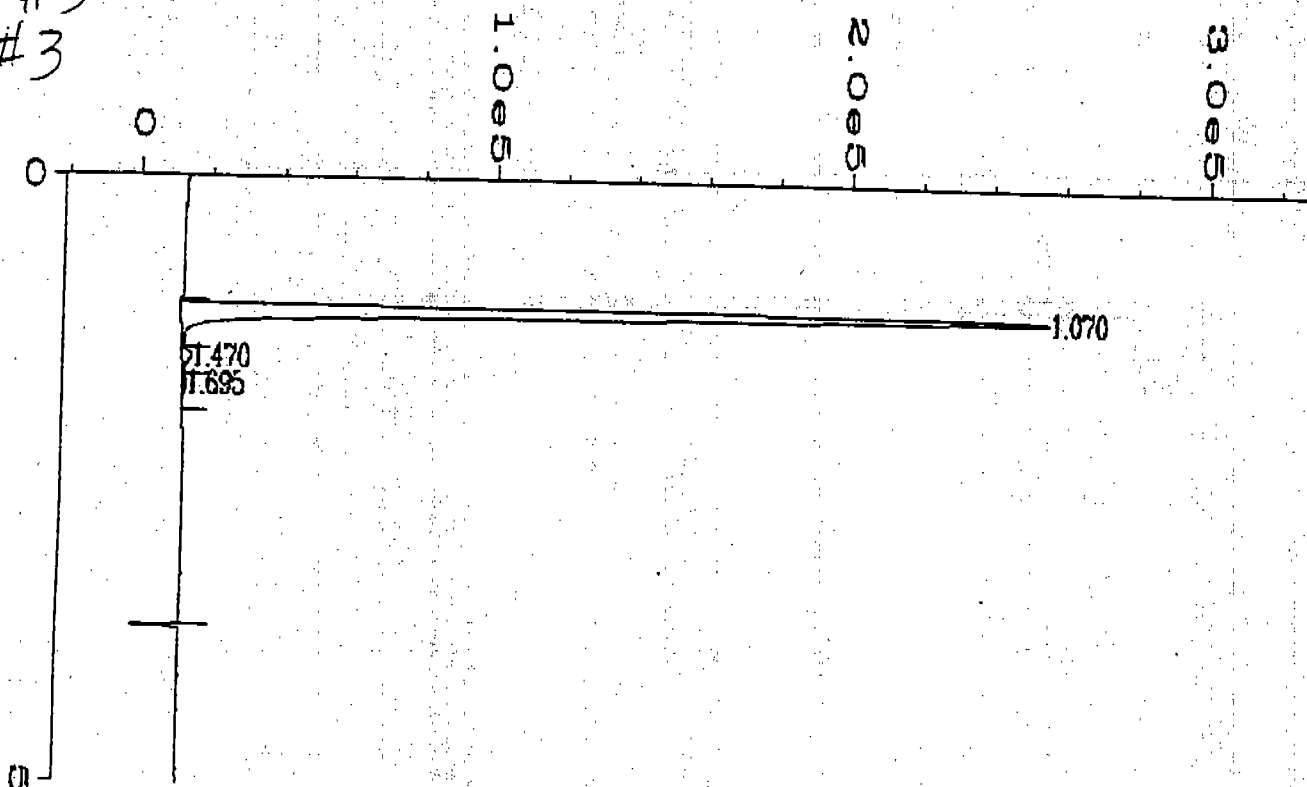
Page Number : 1
 Vial Number :
 Injection Number :
 Sequence Line :
 Instrument Method: MMT5.MTH
 Analysis Method : MMT5.MTH
 Sample Amount : 0
 ISTD Amount :

1 in D:\HPLCHEM\DATA\NV-F0503.D

Time	Area	Type	Width	Ref#	PPM	Name
1.041	1173062	BV	0.077	1-R	2005.703	METHANE

Time Reference Peak	Expected RT	Actual RT	Difference
1	1.060	1.041	-1.8%

ack #1
n #3
j #3



External Standard Report

File Name : C:\HPCHEM\1\DATA\NV-F0504.D
 alor :
 rument : FID/FPD
 le Name :
 Time Bar Code:
 ired on : 14 Dec 93 09:42 PM
 rt Created on: 14 Dec 93 09:48 PM
 Recallib on : 14 Dec 93 08:31 PM
 plier : 1

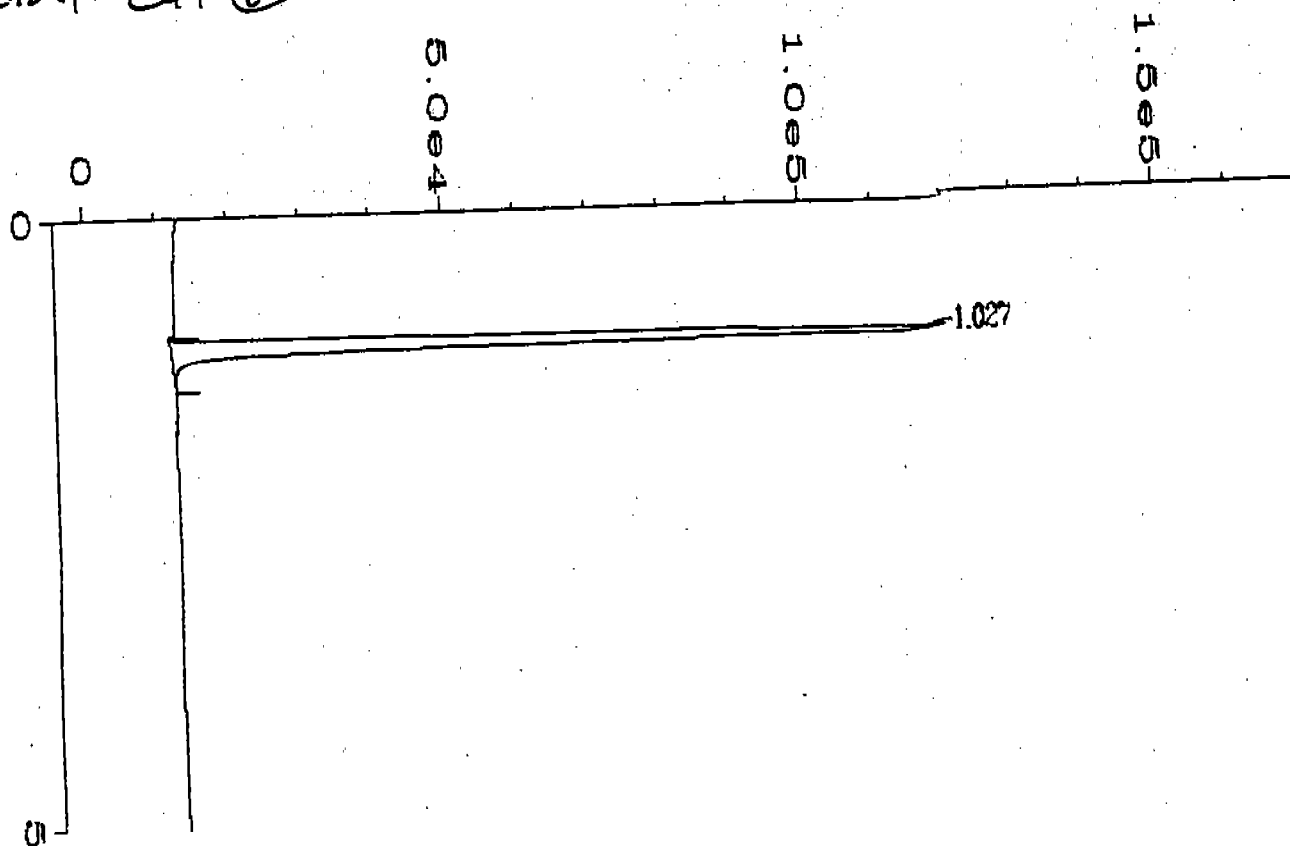
Page Number : 1
 Vial Number :
 Injection Number :
 Sequence Line :
 Instrument Method: MMT5.MTH
 Analysis Method : MMT5.MTH
 Sample Amount : 0
 ISTD Amount :

1 in C:\HPCHEM\1\DATA\NV-F0504.D

Time	Area	Type	Width	Ref#	PPM	Name
1.070	1161044	BV	0.077	1-R	1984.993	METHANE

Time Reference Peak	Expected RT	Actual RT	Difference
1	1.060	1.070	0.9%

In Point Cal (✓)



External Standard Report

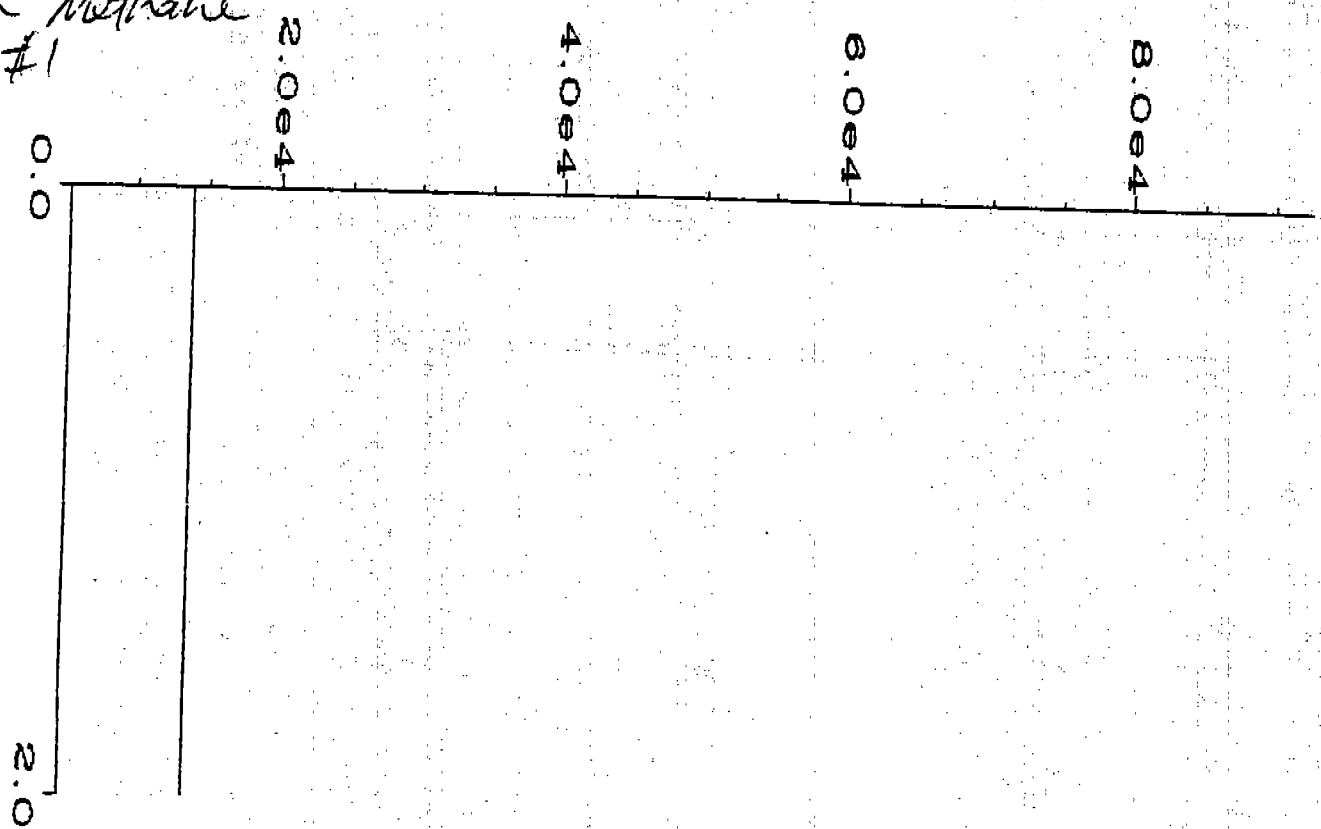
File Name : C:\HPCHEM\1\DATA\NV-F0505.D
Instrument : FID/FPD
Vial Name :
Time Bar Code :
Acquired on : 14 Dec 93 09:51 PM
Report Created on: 14 Dec 93 09:57 PM
Revised on : 14 Dec 93 08:31 PM
Injection : 1

Page Number : 1
Vial Number :
Injection Number :
Sequence Line :
Instrument Method: MMT5.MTH
Analysis Method : MMT5.MTH
Sample Amount : 0
ISTD Amount :

1 in C:\HPCHEM\1\DATA\NV-F0505.D						Name
Time	Area	Type	Width	Ref#	PPM	
1.027	580465	BB	0.086	1-R	984.463	METHANE

Time Reference Peak	Expected RT	Actual RT	Difference
1	1.040	1.027	-1.3%

Cal
in Methane
y#1



External Standard Report

File Name : C:\HFCHEN\1\DATA\NV-F0528.D
 Instrument : FID/FPD
 Time Bar Code:
 Created on : 16 Dec 93 11:09 PM
 File Created on: 16 Dec 93 11:17 PM
 Recalib on : 14 DEC 93 08:31 PM
 Injection : 1

Page Number : 1
 Vial Number :
 Injection Number :
 Sequence Line :
 Instrument Method: BEICHIC.MTH
 Analysis Method : BEICHIC.MTH
 Sample Amount : 0
 ISTD Amount :

1 in C:\HFCHEN\1\DATA\NV-F0528.D

Time	Area	Type	Width	Ref#	PPM	Name
1.070	* not found *	1-R				METHANE

Time Reference Peak	Expected RT	Actual RT	Difference
1	1.070	* not found *	

did not find time reference peak:
 No peak of Number 1's description at 1.070 + 0.027 - 0.027 min.
 all time reference peaks were found

Area Percent Report

File Name : C:\HFCHEN\1\DATA\NV-F0528.D
 Instrument : FID/FPD

Page Number : 1
 Vial Number :

Acquired on : 16 Dec 93 11:09 PM
Report Created on: 16 Dec 93 11:17 PM
Recalculated on : 14 DEC 93 08:31 PM
Multiplier : 1

Instrument Method: BFICHIC.MTH
Analysis Method : BFICHIC.MTH
Sample Amount : 0
ISTD Amount :

1 In C:\HFICHEM\DATA\IV-F0528.D

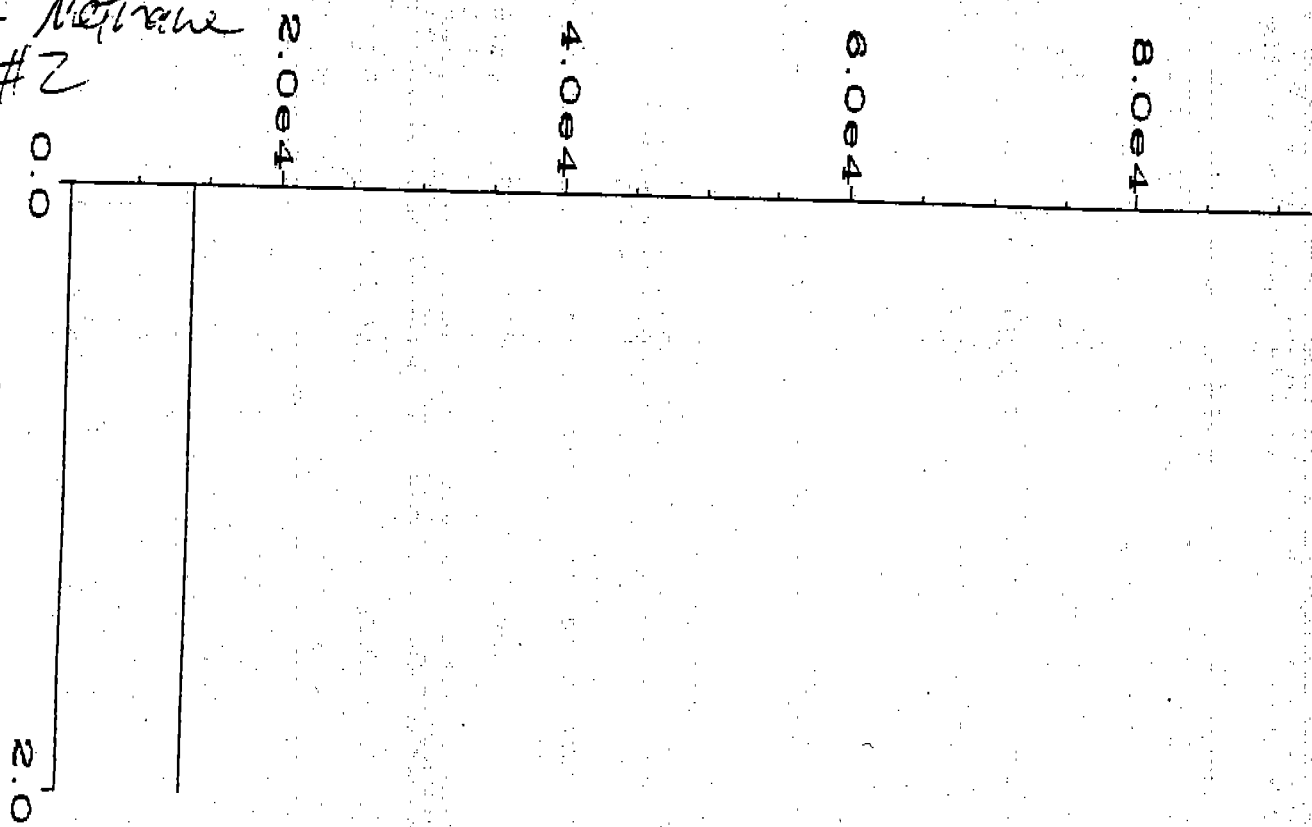
PK#	Ret Time	Area	Height	Type	Width	Area %
-----	----------	------	--------	------	-------	--------

-----	-----	-----	-----	-----	-----	-----
-------	-------	-------	-------	-------	-------	-------

El amount = 0

=====

Cal
in Methane
#2



External Standard Report

File Name : C:\HFICHEM\1\DATA\NV-F0529.D
 Instrument : FID/FPD
 Sample Name :
 Time Bar Code:
 Printed on : 14 Dec 93 19:12 PM
 Report Created on: 14 Dec 93 11:17 PM
 Received on : 14 DEC 93 08:31 PM
 Operator : 1

Page Number : 1
 Vial Number :
 Injection Number :
 Sequence Line :
 Instrument Method: PFICHIC.MTH
 Analysis Method : BF7CHIC.MTH
 Sample Amount : 0
 ISTD Amount :

1 in C:\HFICHEM\1\DATA\NV-F0529.D				
Time	Area	Type	Width	Ref#
1.070	* not found *	1-R		

METHANE

Time Reference Peak	Expected RT	Actual RT	Difference
1	1.070	* not found *	

do not find time reference peak:

No peak of Number 1's description at 1.070 + 0.027 - 0.027 min.
 all time reference peaks were found

Area Percent Report

File Name : C:\HFICHEM\1\DATA\NV-F0529.D
 Instrument : FID/FPD
 Sample Name :

Page Number : 1
 Vial Number :
 Injection Number :

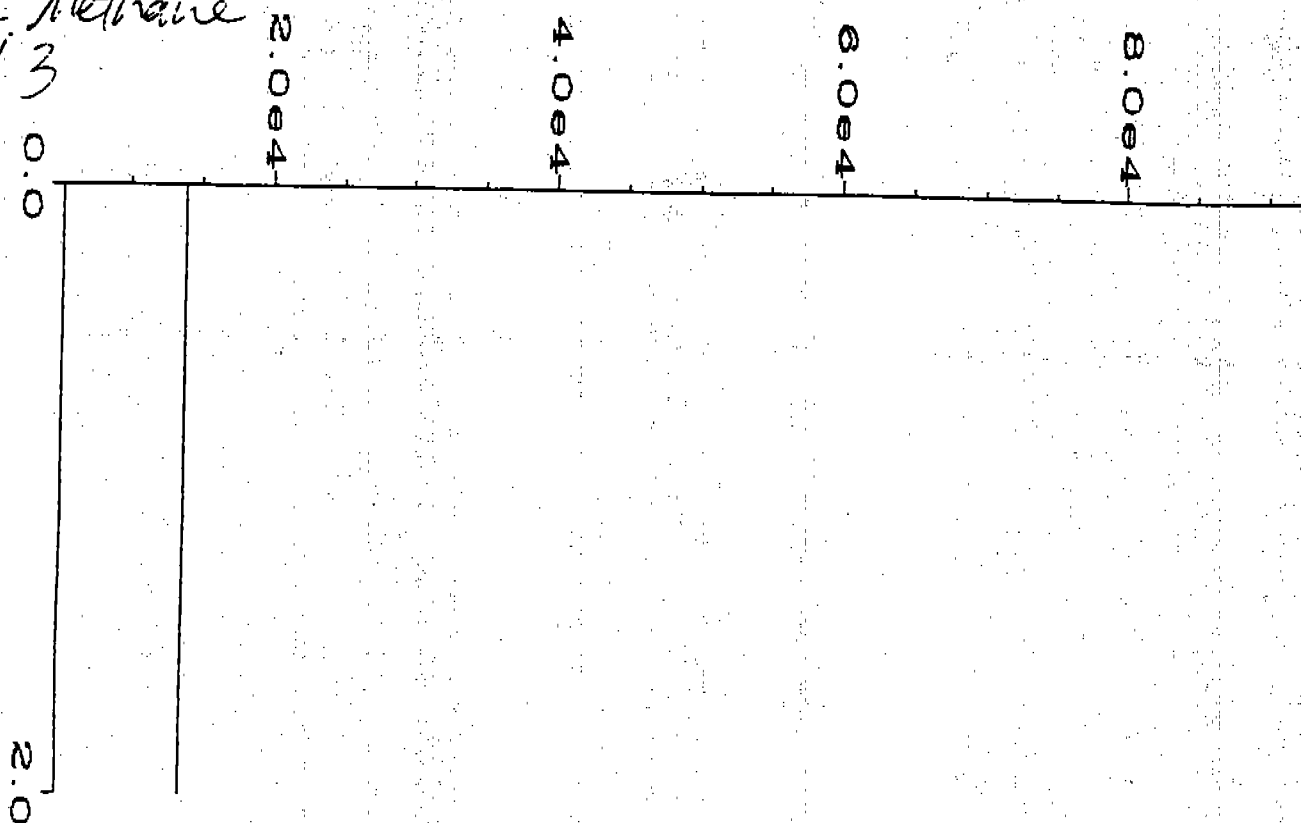
Printed on : 16 Dec 93 11:12 PM
Report Created on: 16 Dec 93 11:17 PM
Recalib on : 14 DEC 93 08:31 PM
Injection : 1

Instrument Method: BPICHC.MTH
Analysis Method : BPICHC.MTH
Sample Amount : 0
ISTD Amount :

1 in C:\VHPCHEM\DATA\NV-FOI27.D
Peak Rel. Time Area Height Type Width Area %

Amount = 0

Cal
in Methane
#3



External Standard Report

File Name : C:\HPCHEM\1\DATA\NV-F0530.D
 Instrument : FID/FPD
 Sample Name :
 Time Bar Code:
 Printed on : 16 Dec 93 11:18 PM
 Report Created on: 16 Dec 93 11:20 PM
 Recalibration : 14 DEC 93 09:51 PM
 Multiplier : 1

Page Number : 1
 Vial Number :
 Injection Number :
 Sequence Line :
 Instrument Method: BFICHC.MTH
 Analysis Method : BFICHC.MTH
 Sample Amount : 0
 ISTD Amount :

1 in C:\HPCHEM\1\DATA\NV-F0530.D

Time	Area	Type	Width	Ref#	PPM	Name
1.070	* not found *			1-R		METHANE

Time Reference Peak	Expected RT	Actual RT	Difference
1	1.070	* not found *	

Did not find time reference peak:

No peak of Number 1's description at 1.070 ± 0.027 - 0.027 min.
 all time reference peaks were found

Area Percent Report

File Name : C:\HPCHEM\1\DATA\NV-F0530.D
 Instrument : FID/FPD

Page Number : 1
 Vial Number :

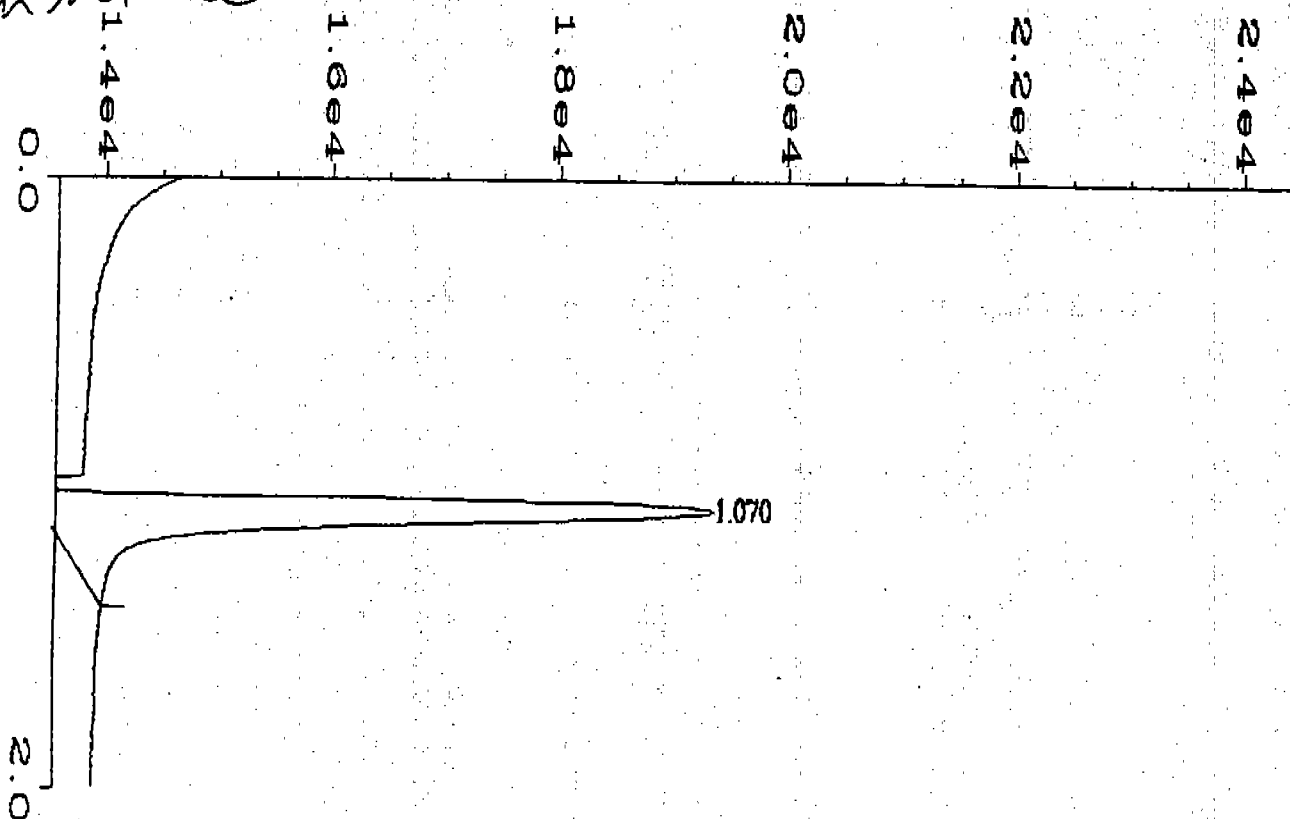
Printed on : 16 Dec 93 11:18 PM
Report Created on: 16 Dec 93 11:20 PM
Revised on : 14 DEC 93 08:31 PM
Printer : 1

Instrument Method: MTH.MTH
Analysis Method : BFIC.MTH
Sample Amount : 0
ISTD Amount :

1 in C:\HPCHEM\1\DATA\NV-F0530.D
PK# Ret Time Area Height Type Width Area %

amount = 0

Cal
ppm Methane



External Standard Report

File Name : C:\NHPCHEM\1\DATA\NV-F0531.D
 Detector : FID/FPD
 Sample Name :
 Time Bar Code:
 Acquired on : 16 Dec 93 11:25 PM
 Report Created on: 16 Dec 93 11:28 PM
 Report Valid on : 14 DEC 93 08:31 PM
 Multiplier : 1

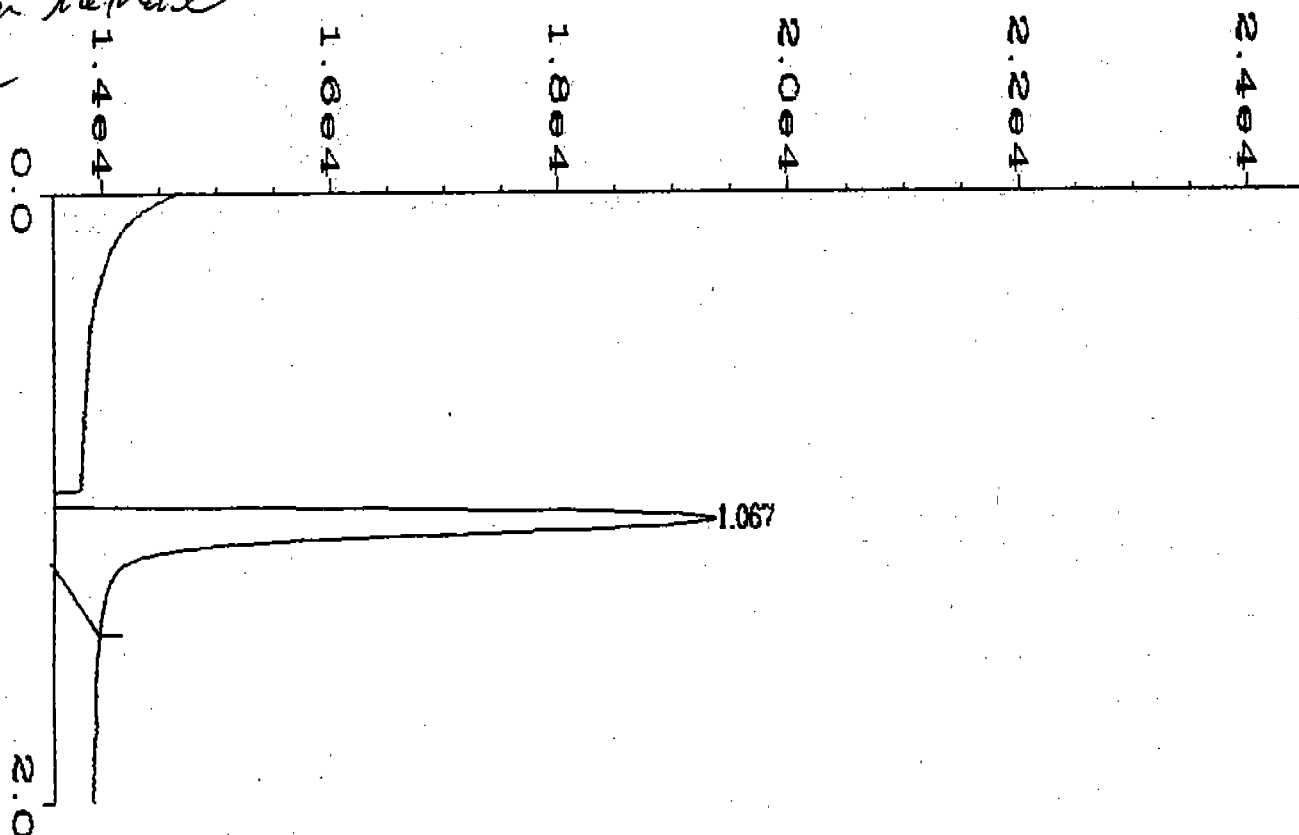
Page Number : 1
 Vial Number :
 Injection Number :
 Sequence Line :
 Instrument Method: EFICHIC.MTH
 Analysis Method : EFICHIC.MTH
 Sample Amount : 0
 ISTD Amount :

1 in C:\NHPCHEM\1\DATA\NV-F0531.D

Time	Area	Type	Width	Ref#	PPM	Name
1.070	36163	BB	0.097	1-R	47.050	METHANE

Time Reference Peak	Expected RT	Actual RT	Difference
1	1.070	1.070	0.0%

Vial #2 from Methane



External Standard Report

File Name : C:\HPCHEM\1\DATA\NV-F0532.D
 Detector :
 Instrument : FID/FPD
 Sample Name :
 Time Bar Code:
 Printed on : 16 Dec 93 11:29 PM
 Report Created on: 16 Dec 93 11:32 PM
 Sample Recal on : 14 DEC 93 08:31 PM
 Syllor : 1

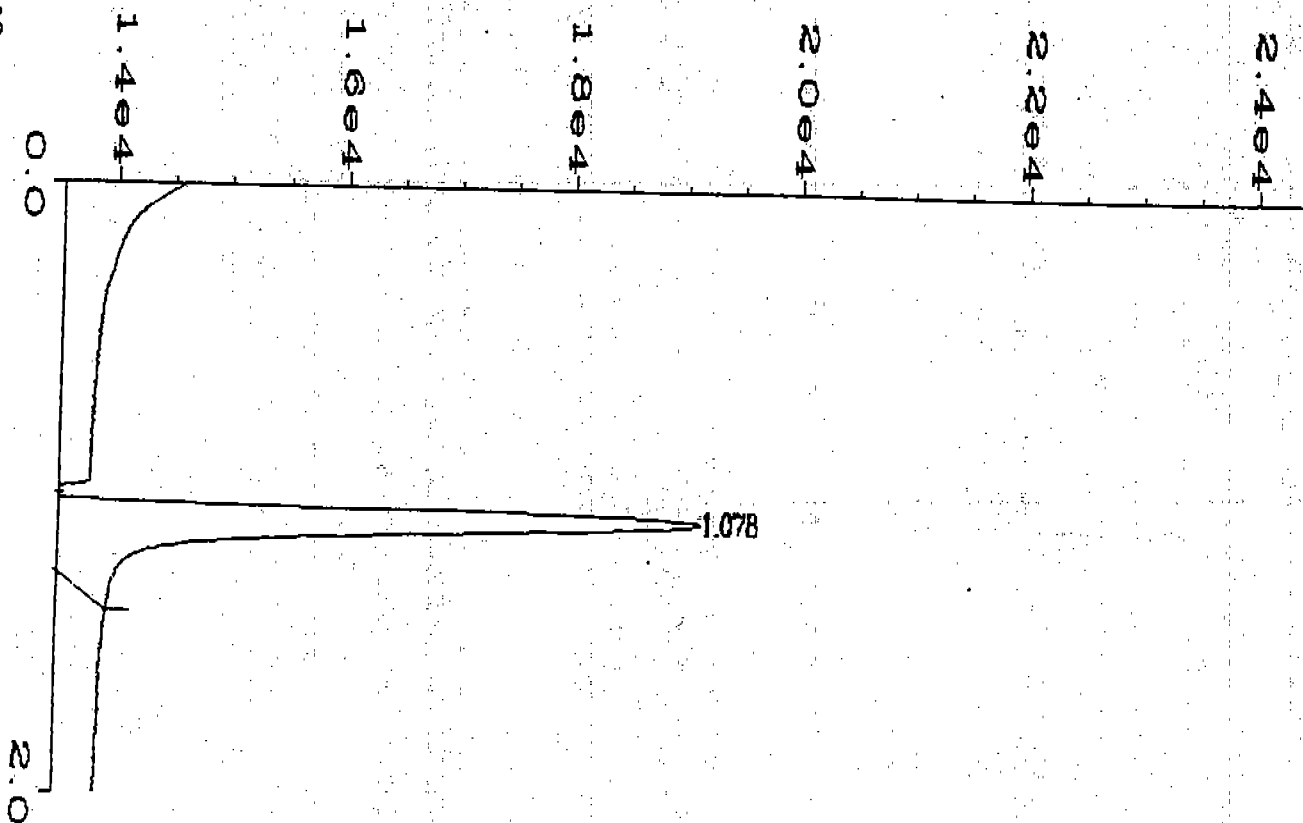
Page Number : 1
 Vial Number :
 Injection Number :
 Sequence Line :
 Instrument Method: BF1CHIC.MTH
 Analysis Method : BF1CHIC.MTH
 Sample Amount : 0
 ISTD Amount :

1 in C:\HPCHEM\1\DATA\NV-F0532.D

Time	Area	Type	Width	Ref#	PPM	Name
1.067	39907	BB	0.103	1-R	52.902	METHANE

Time Reference Peak	Expected RT	Actual RT	Difference
1	1.070	1.067	-0.3%

91
 3
 ifm Methane



External Standard Report

File Name : C:\HPCHEM\1\DATA\NV-F0535.D
 ation :
 Instrument : FID/FPD
 File Name :
 Time Base Code:
 Acquired on : 16 Dec 93 11:41 PM
 Report Created on: 16 Dec 93 11:42 PM
 Recalib on : 14 DEC 93 08:31 PM
 Injector : 1

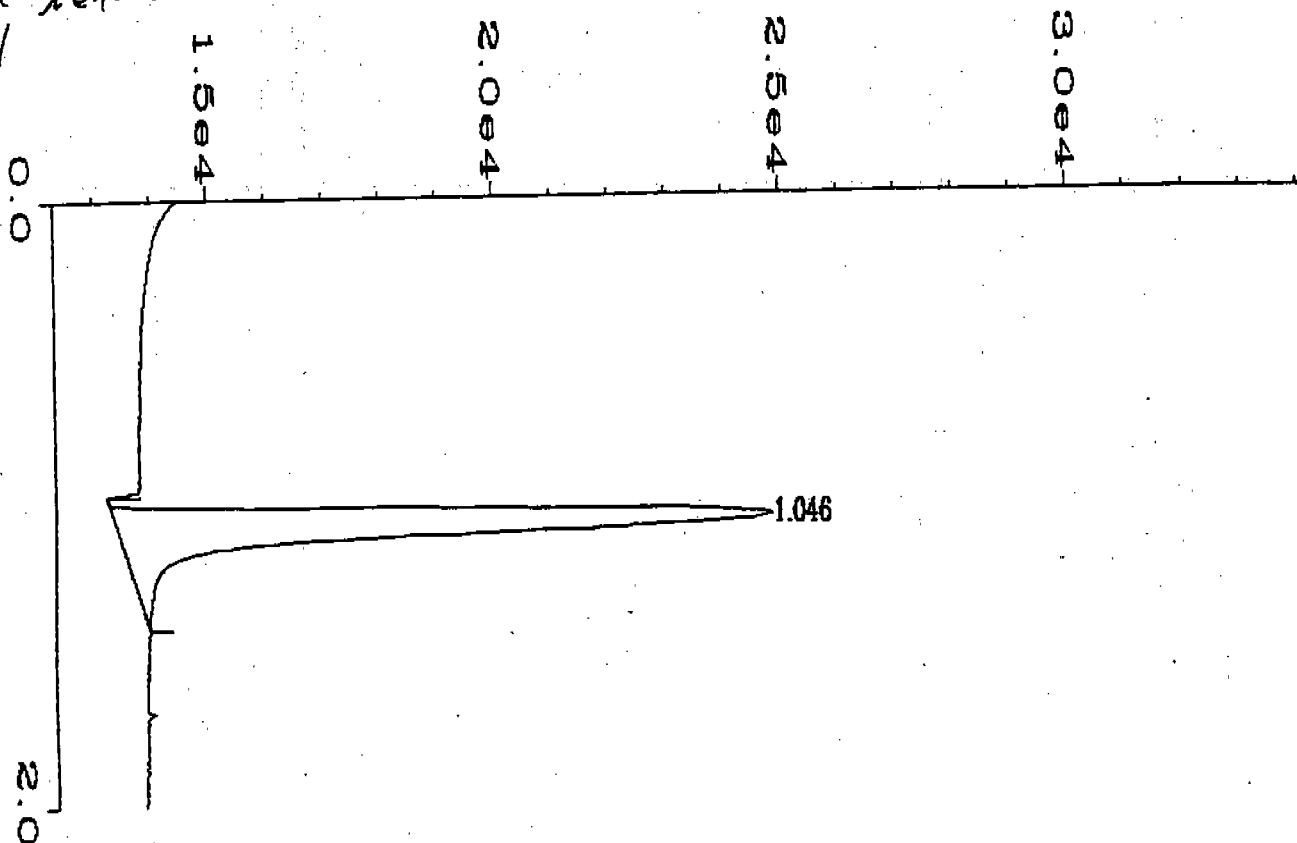
Page Number : 1
 Vial Number :
 Injection Number :
 Sequence Line:
 Instrument Method: E01CHIC.MTH
 Analysis Method : BF1CHIC.MTH
 Sample Amount : 0
 ISTD Amount :

1 in C:\HPCHEM\1\DATA\NV-F0535.D

Time	Area	Type	Width	Ref#	PPM	Name
1.078	42273	BB	0.102	1-R	56.979	METHANE

Time Reference Peak	Expected RT	Actual RT	Difference
1	1.070	1.078	0.7%

Cal
ppm Methane
#1



External Standard Report

File Name : C:\HFICHEM\1\DATA\NV-F0536.D
Ratio :
Instrument : FID/FPD
Sample Name :
Time Bar Code :
Acquired on : 16 Dec 93 11:45 PM
Report Created on: 16 Dec 93 11:48 PM
Last Recalib on : 14 DEC 93 08:31 PM
Multiplier : 1

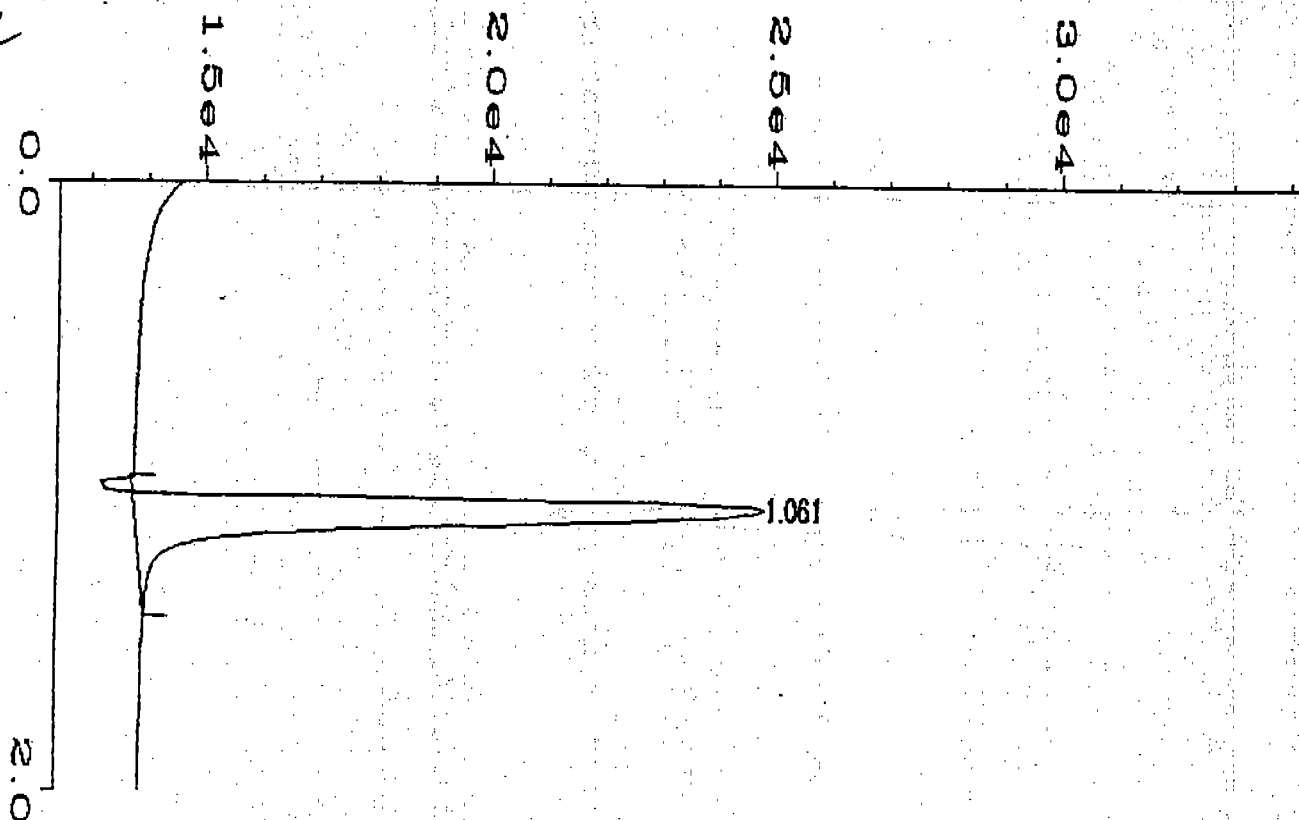
Page Number : 1
Vial Number :
Injection Number :
Sequence Line :
Instrument Method: BFICID.MTH
Analysis Method : BFICID.MTH
Sample Amount : 0
ISTD Amount :

1 in C:\HFICHEM\1\DATA\NV-F0536.D

Time	Area	Type	Width	Ref#	PPM	Name
1.046	68786	BB	0.095	1-R	102.670	METHANE

Time Reference Peak	Expected RT	Actual RT	Difference
1	1.070	1.046	-2.2%

Cal
Mm Methane
#2



External Standard Report

File Name : C:\HPCHEM\1\DATA\NV-F0539.D

Instrument : FID/FPD

Sample Name :

Time Bar Code:

Printed on : 16 Dec 93 11:56 PM

Report Created on: 16 Dec 93 11:59 PM

Recalibration : 14 DEC 93 08:31 PM

Multiplier : 1

Page Number : 1

Vial Number :

Injection Number :

Sequence Line :

Instrument Method: BFIC10.MTH

Analysis Method : BFIC10.MTH

Sample Amount : 0

ISTD Amount :

1 in C:\HPCHEM\1\DATA\NV-F0539.D

Time	Area	Type	Width	Ref#	PPM	Name
1.061	63378	BB	0.092	1-R	93.349	METHANE

Time Reference Peak

Expected RT

Actual RT

Difference

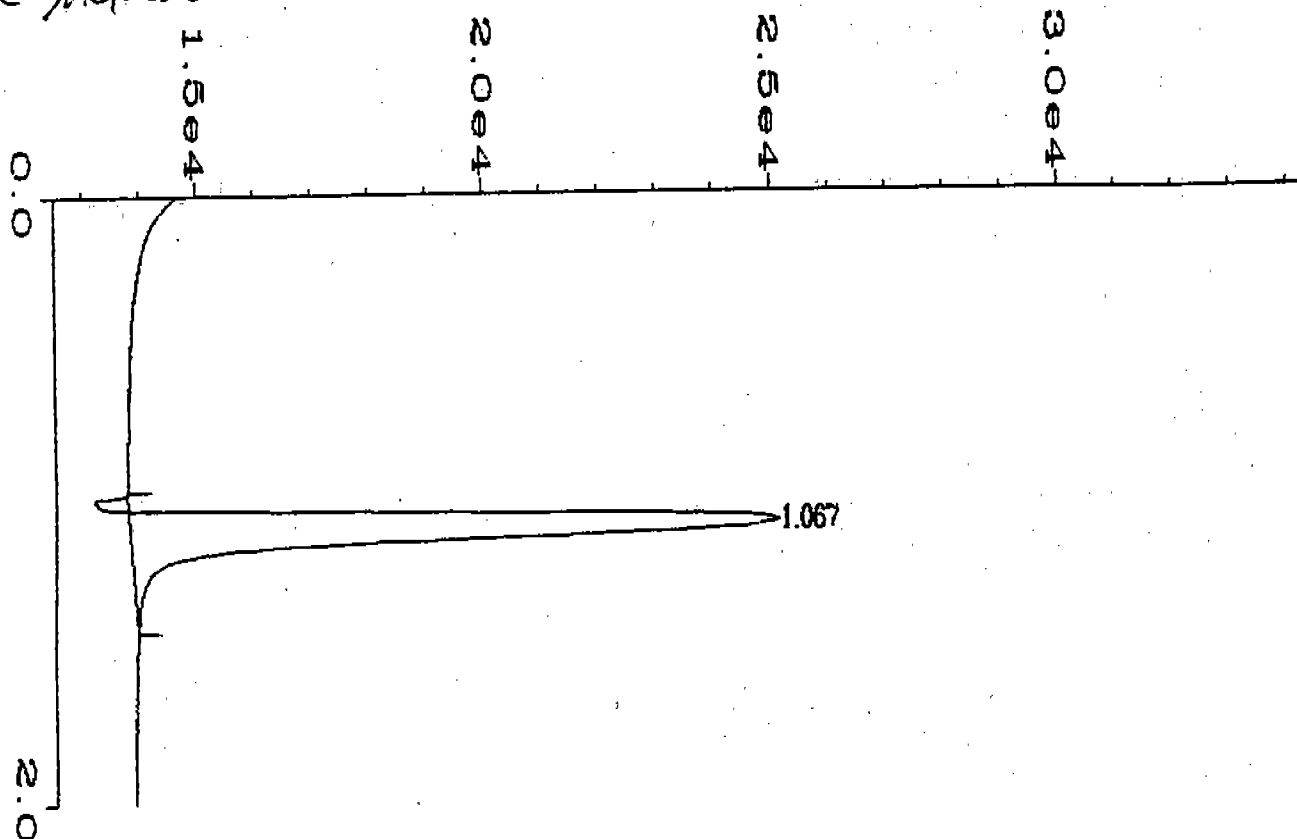
1

1.070

1.061

-0.8%

21
ppm Methane
E3



External Standard Report

File Name : C:\HPCHEM\1\DATA\NV-F0540.D
 ator :
 ument : FID/FPD
 le Name :
 Time Bar Code:
 ired on : 17 Dec 93 00:00 AM
 t Created on: 17 Dec 93 00:02 AM
 Recalib on : 14 DEC 93 08:31 PM
 plier : 1

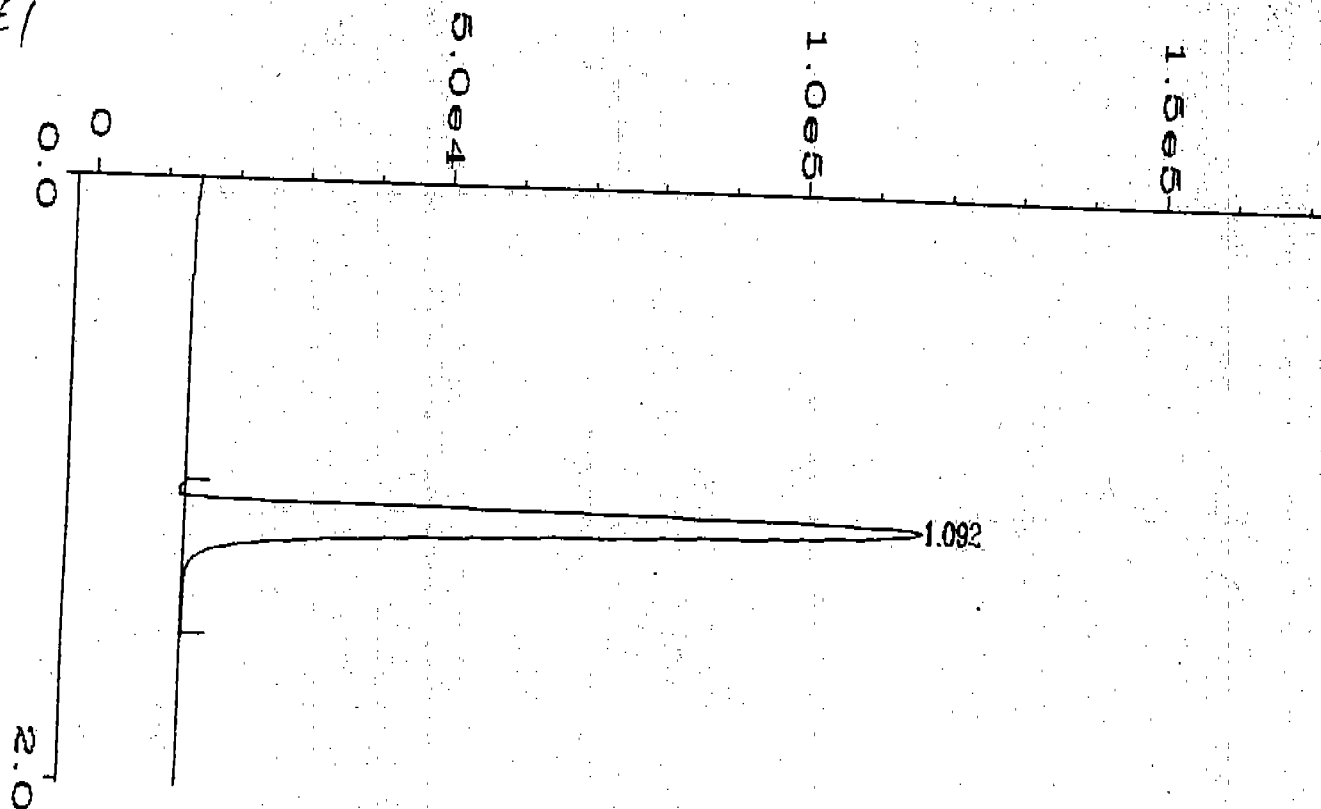
Page Number : 1
 Vial Number :
 Injection Number:
 Sequence Line :
 Instrument Method: BF1CH1C.MTH
 Analysis Method : BF1CH1C.MTH
 Sample Amount : 0
 ISTD Amount :

1 in C:\HPCHEM\1\DATA\NV-F0540.D

Time	Area	Type	Width	Ref#	PPM	Name
1.067	66142	BB	0.094	1-R	98.113	METHANE

Time Reference Peak	Expected RT	Actual RT	Difference
1	1.070	1.067	-0.3%

Si!
in Methane
#1



External Standard Report

File Name : C:\HPCHEM\1\DATA\NV-F0542.D
ator :
Instrument : FID/FPD
Sample Name :
Time Bar Code :
Printed on : 17 Dec 93 00:08 AM
Port Created on: 17 Dec 93 00:11 AM
Recalib. on : 14 DEC 93 08:31 PM
Multiplier : 1

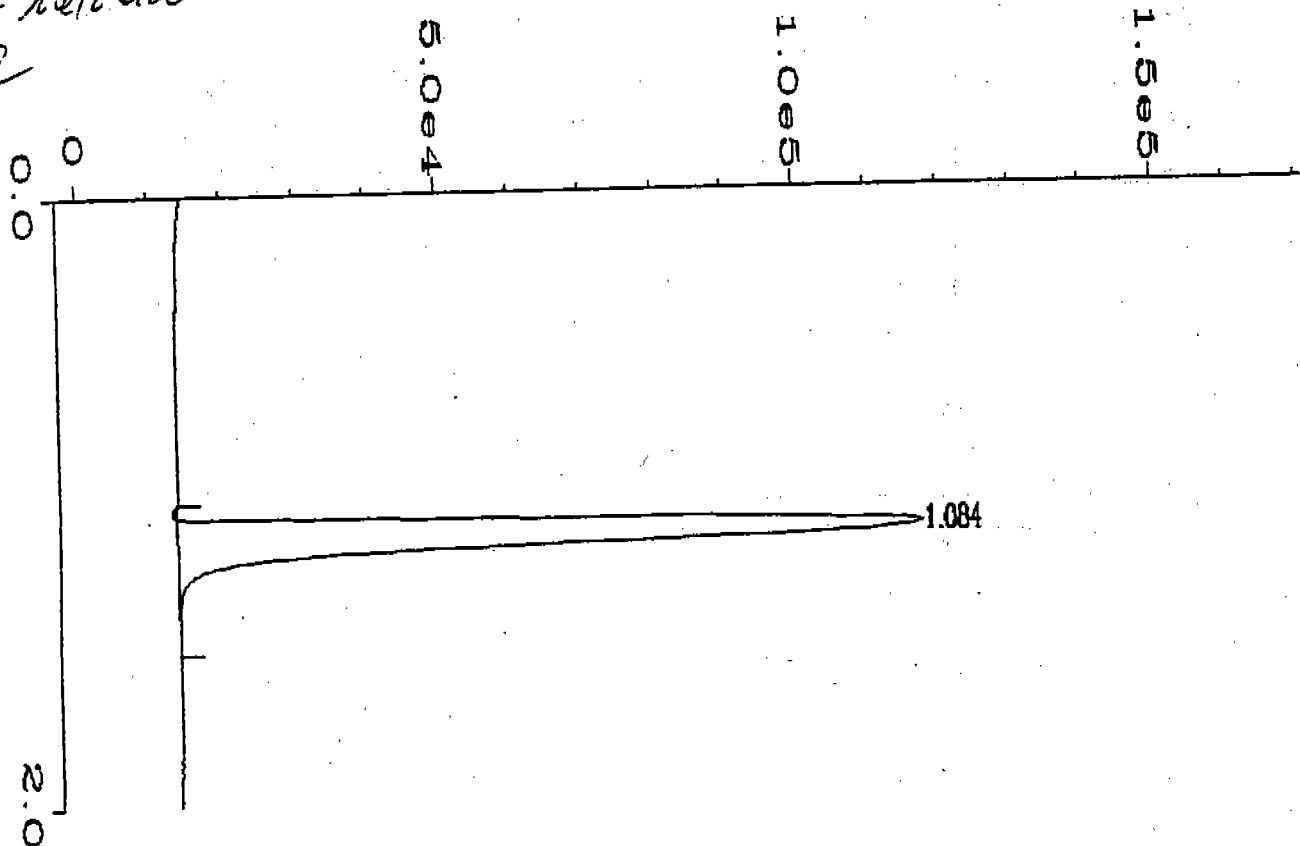
Page Number : 1
Vial Number :
Injection Number :
Sequence Line :
Instrument Method: BF1CH1C.MTH
Analysis Method : BF1CH1C.MTH
Sample Amount : 0
ISTD Amount :

1 in C:\HPCHEM\1\DATA\NV-F0542.D

Time	Area	Type	Width	Ref#	PPM	Name
1.092	546093	BP	0.088	1-R	959.696	METHANE

Time Reference Peak	Expected RT	Actual RT	Difference
1	1.075	1.092	1.6%

Cal
from Methane
#2



External Standard Report

File Name : C:\HPCHEM\1\DATA\NV-F0543.D
 Detector :
 Instrument : FID/FPD
 Sample Name :
 Time Bar Code:
 Inj. Port : 17 Dec 93 00:12 AM
 Port Created on: 17 Dec 93 00:15 AM
 Recalib on : 14 DEC 93 08:33 PM
 Multiplier : 1

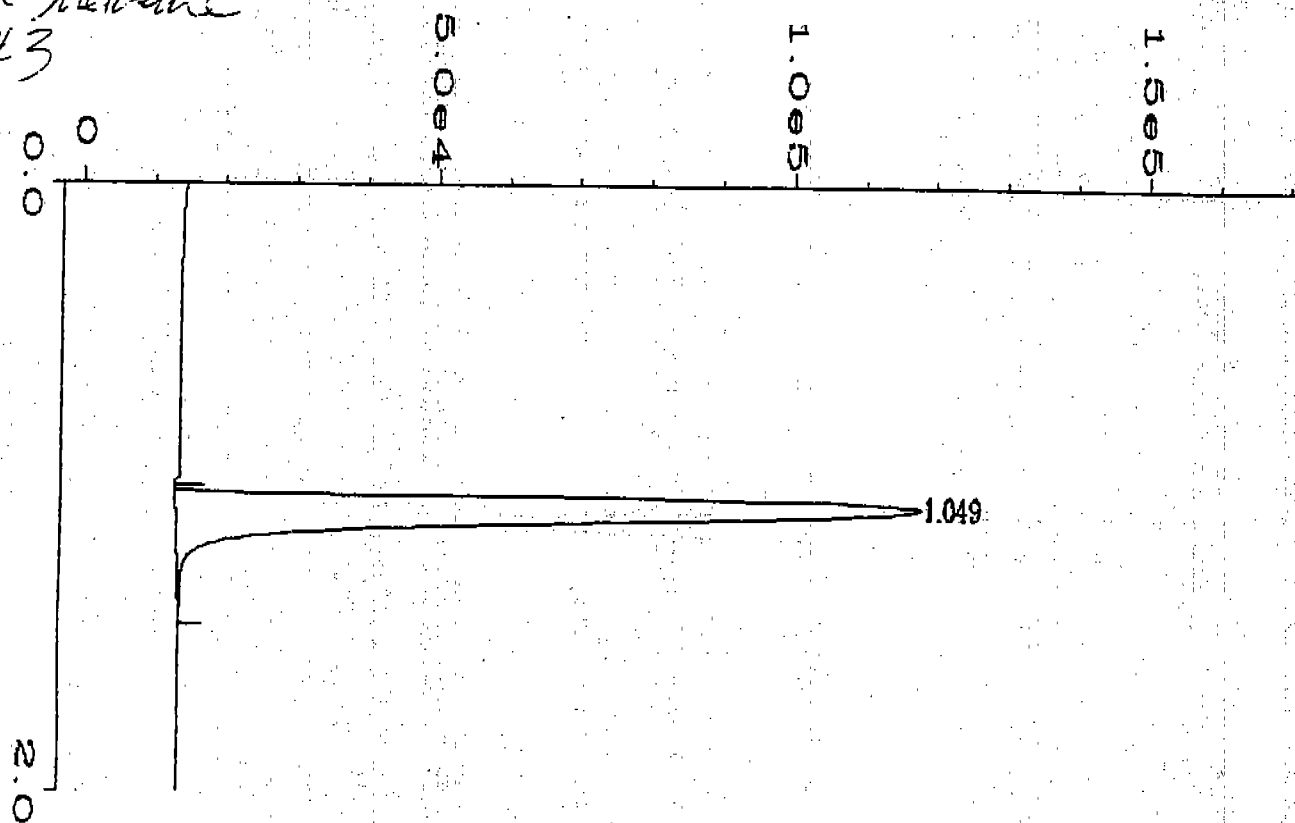
Page Number : 1
 Vial Number :
 Injection Number :
 Sequence Line :
 Instrument Method: BFIC11C.MTH
 Analysis Method : BFIC11C.MTH
 Sample Amount : 0
 ISTD Amount :

1 in C:\HPCHEM\1\DATA\NV-F0543.D

Time	Area	Type	Width	Ref#	FPM	Name
1.084	570145	BE	0.089	1-R	966.678	METHANE

Time Reference Peak	Expected RT	Actual RT	Difference
1	1.075	1.084	0.8%

Cal
from Methane
#3



External Standard Report

File Name : C:\HPCHEM\1\DATA\NV-F0544.D
 Motor :
 Instrument : FID/EPD
 Sample Name :
 Type Ref. Code:
 Acquisition on: 17 Dec 93 00:16 AM
 Data Acquisition on: 17 Dec 93 00:18 AM
 Review on: 14 DEC 93 08:31 PM
 Amplifier : 1

Page Number : 1
 Vial Number :
 Injection Number :
 Sequence Line :
 Instrument Method: BFICHC.MTH
 Analysis Method : BFICHC.MTH
 Sample Amount : 0
 ISTD Amount :

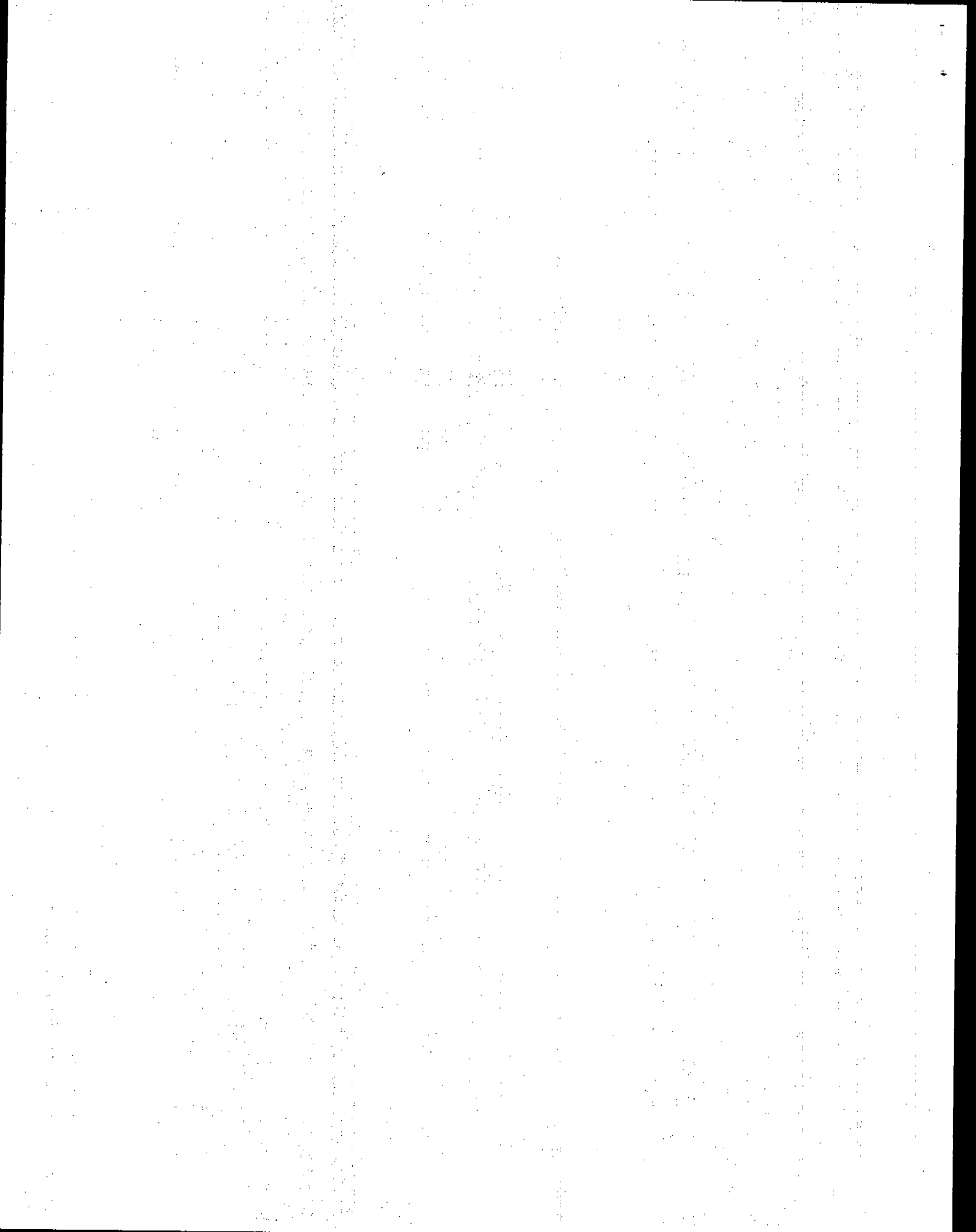
1 in C:\HPCHEM\1\DATA\NV-F0544.D

Time	Area	Type	Width	Ref#	PPM	Name
1.049	582404	BB	0.090	1-R	987.804	METHANE

Time	Reference Peak	Expected RT	Actual RT	Difference
1		1.075	1.049	-2.4%

APPENDIX D

V.E. OBSERVATION DATA AND CERTIFICATION SHEET

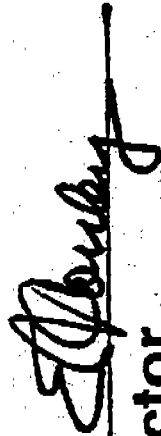


United States Environmental Protection Agency Region 1 Environmental Services Division



Certifies That
TIMOTHY J. SENG

Meets the qualifications prescribed by the Code of Federal Regulations
Vol.40; Part 60, Method 9 for the evaluation of Visible Emissions
Issued this 5th Day of October 1993.


Director

Environmental Services Division


Course Instructor

This Certificate Expires April 5th 1994.

Visible Emission Observation Form

Company Name BFI
 Street Address 845 Burnett Road
 City Chicopee State MA Zip 01020
 Phone (key contact) (413) 592-8168 Source ID Number Stack #1

Process Equipment Landfill gas fired generator Operating Mode Full
 Control Equipment Muffler Operating Mode Full/Normal

Describe Emission Point Muffler Vent (Horizontal)
 Height Above Ground Level 23' Height Relative to Observer Start 17' End 17'
 Distance from Observer Start 100' End 100' Direction from Observer Start NW End NW

Describe Emissions Start No Physical Char. End No Physical Char.
 Emission Color Start None End None If Water Droplet Plume Attached ☐ Detached ☐
 Point in the Plume at which Opacity was Determined Start End of outlet End End of outlet

Describe Plume Background Start Overcast White Sky End Overcast White Sky
 Background Color Start White End White Sky Conditions Start Overcast End Overcast
 Wind Speed Start 10mph End 10mph Wind Direction Start 0° N End 0° N
 Ambient Temp Start 45°F End 45°F Wet Bulb Temp 38°F RH Percent 50

Stack with Plume ☒
 Sun ☒
 Wind ☒
 Source Layout Sketch
 Draw North Arrow
 Emission Point
 Observer's Position
 Sun Location Line

Observation date <u>14 Dec 93</u>				Start Time <u>1100</u>		End Time <u>1130</u>	
MIN	SEC	0	15	30	45	Comments	
1		0	0	0	0		
2		0	0	0	0		
3		0	0	0	0		
4		0	0	0	0		
5		0	0	0	0		
6		0	0	0	0		
7		0	0	0	0		
8		0	0	0	0		
9		0	0	0	0		
10		0	0	0	0		
11		0	0	0	0		
12		0	0	0	0		
13		0	0	0	0		
14		0	0	0	0		
15		0	0	0	0		
16		0	0	0	0		
17		0	0	0	0		
18		0	0	0	0		
19		0	0	0	0		
20		0	0	0	0		
21		0	0	0	0		
22		0	0	0	0		
23		0	0	0	0		
24		0	0	0	0		
25		0	0	0	0		
26		0	0	0	0		
27		0	0	0	0		
28		0	0	0	0		
29		0	0	0	0		
30		0	0	0	0		

Observer's Name (print) Timothy J. Senger
 Observer's Signature Timothy J. Senger
 Organization TRC Environmental Corp.
 Certified By EPA Region 1
 Date 14 Dec 93
 Continued on VEO Form Number 5 Oct 93

TRC

Visible Emission Observation Form

Company Name <u>BFI</u>		
Street Address <u>845 Burnett Road</u>		
City <u>Chicopee</u>	State <u>MA</u>	Zip <u>01020</u>
Phone (key contact) <u>(413) 592-8168</u>	Source ID Number <u>Stack #1</u>	

Process Equipment <u>Landfill gas fired generator</u>	Operating Mode <u>Full</u>
Control Equipment <u>Muffler</u>	Operating Mode <u>Full/Normal</u>

Describe Emission Point <u>Muffler Vent (Horizontal)</u>	
Height Above Ground Level <u>23'</u>	Height Relative to Observer Start <u>17'</u> End <u>17'</u>
Distance from Observer Start <u>100'</u> End <u>100'</u>	Direction from Observer Start <u>NW</u> End <u>NW</u>

Describe Emissions Start <u>No Physical Char.</u> End <u>No Physical Char.</u>	
Emission Color Start <u>None</u> End <u>None</u>	If Water Droplet Plume Attached ☐ Detached ☐
Point in the Plume at which Opacity was Determined Start <u>End of outlet</u> End <u>End of outlet</u>	

Describe Plume Background Start <u>Overcast White Sky</u> End <u>Overcast White Sky</u>	
Background Color Start <u>White</u> End <u>White</u>	Sky Conditions Start <u>Overcast</u> End <u>Overcast</u>
Wind Speed Start <u>10 mph</u> End <u>15 mph</u>	Wind Direction Start <u>0° N</u> End <u>0° N</u>
Ambient Temp Start <u>45°F</u> End <u>44°F</u>	Wet Bulb Temp RH, Percent Start <u>37°F</u> End <u>50</u>

Stack with Plume	Source Layout Sketch	Draw North Arrow
Sun	Emission Point	
Wind	Observer's Position	
Sun Location Line		

Additional Information <u>Stack #1 Run #1</u>
<u>Sheet 2 of 2</u>

Observation date <u>14 Dec 93</u>		Start Time <u>1130</u>		End Time <u>1200</u>	
SEC MIN	0	15	30	45	Comments
1	0	0	0	0	
2	0	0	0	0	
3	0	0	0	0	
4	0	0	0	0	
5	0	0	0	0	
6	0	0	0	0	
7	0	0	0	0	
8	0	0	0	0	
9	0	0	0	0	
10	0	0	0	0	
11	0	0	0	0	
12	0	0	0	0	
13	0	0	0	0	
14	0	0	0	0	
15	0	0	0	0	
16	0	0	0	0	
17	0	0	0	0	
18	0	0	0	0	
19	0	0	0	0	
20	0	0	0	0	
21	0	0	0	0	
22	0	0	0	0	
23	0	0	0	0	
24	0	0	0	0	
25	0	0	0	0	
26	0	0	0	0	
27	0	0	0	0	
28	0	0	0	0	
29	0	0	0	0	
30	0	0	0	0	

Observer's Name (print) <u>Timothy J. Senger</u>
Observer's Signature <u>Timothy J. Senger</u> <u>14 Dec 93</u>
Organization <u>TRC Environmental Corp.</u>
Certified By <u>EPA Region 1</u> <u>5 Oct 93</u>
Continued on VEO Form Number <u> </u>

TRC

Visible Emission Observation Form

Company Name BFI
 Street Address 845 Burnett Road
 City Chicopee State MA Zip 01020
 Phone (key contact) (413) 592-8168 Source ID Number Stack #1

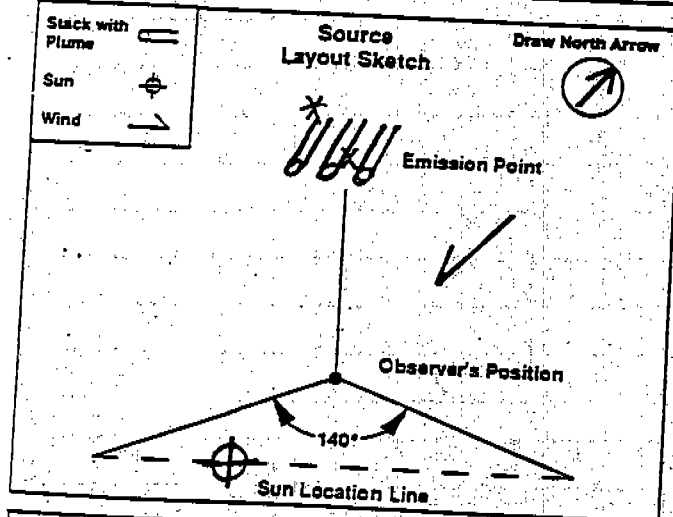
Process Equipment Landfill gas-fired generator Operating Mode Full
 Control Equipment Muffler Operating Mode Full/Normal

Describe Emission Point
Muffler Vent (Horizontal)

Height Above Ground Level 23' Height Relative to Observer
 Start 17' End 17'
 Distance from Observer
 Start 100' End 100' Direction from Observer
 Start NW End NW

Describe Emissions
 Start No Physical Char. End No Physical Char.
 Emission Color None If Water Droplet Plume
 Start None End None Attached ☐ Detached ☐
 Point in the Plume at which Opacity was Determined
 Start End of outlet End End of outlet

Describe Plume Background
 Start Overcast white sky End Overcast white sky
 Background Color White Sky Conditions Overcast
 Start White End White Start Overcast End Overcast
 Wind Speed 15mph Wind Direction 0° N
 Start 15mph End 15mph Start 0° N End 0° N
 Ambient Temp 44°F Wet Bulb Temp 36°F RH, Percent 50
 Start 44°F End 43°F Start 36°F End 30



Additional Information Stack #1 Run #2
Sheet 1 of 2

Observation date <u>14 Dec 93</u>				Start Time <u>1200</u>	End Time <u>1230</u>	
MIN	SEC	0	15	30	45	Comments
1		0	0	0	0	
2		0	0	0	0	
3		0	0	0	0	
4		0	0	0	0	
5		0	0	0	0	
6		0	0	0	0	
7		0	0	0	0	
8		0	0	0	0	
9		0	0	0	0	
10		0	0	0	0	
11		0	0	0	0	
12		0	0	0	0	
13		0	0	0	0	
14		0	0	0	0	
15		0	0	0	0	
16		0	0	0	0	
17		0	0	0	0	
18		0	0	0	0	
19		0	0	0	0	
20		0	0	0	0	
21		0	0	0	0	
22		0	0	0	0	
23		0	0	0	0	
24		0	0	0	0	
25		0	0	0	0	
26		0	0	0	0	
27		0	0	0	0	
28		0	0	0	0	
29		0	0	0	0	
30		0	0	0	0	

Observer's Name (print) Timothy J. Senger
 Observer's Signature Timothy J. Senger 14 Dec 93
 Organization TRC Environmental Corp.
 Certified By EPA Region 1 5 Oct 93
 Continued on VED Form Number

TRC

Visible Emission Observation Form

Company Name BFI

Street Address 845 Burnett Road

City Chicopee State MA Zip 01020

Phone (key contact) (413) 592-8168 Source ID Number Stack #1

Process Equipment Landfill gas fired generator Operating Mode Full

Control Equipment Muffler Operating Mode Full/Normal

Describe Emission Point Muffler Vent (Horizontal)

Height Above Ground Level 23' Height Relative to Observer Start 17' End 17'

Distance from Observer Start 100' End 100' Direction from Observer Start NW End NW

Describe Emissions Start No Physical Char. End No Physical Char.

Emission Color Start None End None If Water Droplet Plume Attached ☐ Detached ☐

Point in the Plume at which Opacity was Determined Start End of outlet End End of outlet

Describe Plume Background Start Overcast White Sky End Overcast White Sky

Background Color Start White End White Sky Conditions Start Overcast End Overcast

Wind Speed Start 15mph End 15mph Wind Direction Start 0° N End 0° N

Ambient Temp. Start 43°F End 43°F Wet Bulb Temp 36°F RH, Percent 50

Stack with Plume ☐ Sun ☒ Wind ☒

Source Layout Sketch

Draw North Arrow

Emission Point

Observer's Position

Sun Location Line

Additional Information Stack #1 Run #2

Sheet 2 of 2

Observation date <u>14 Dec 93</u>		Start Time <u>1230</u>		End Time <u>1300</u>	
sec	0	15	30	45	Comments
1	0	0	0	0	
2	0	0	0	0	
3	0	0	0	0	
4	0	0	0	0	
5	0	0	0	0	
6	0	0	0	0	
7	0	0	0	0	
8	0	0	0	0	
9	0	0	0	0	
10	0	0	0	0	
11	0	0	0	0	
12	0	0	0	0	
13	0	0	0	0	
14	0	0	0	0	
15	0	0	0	0	
16	0	0	0	0	
17	0	0	0	0	
18	0	0	0	0	
19	0	0	0	0	
20	0	0	0	0	
21	0	0	0	0	
22	0	0	0	0	
23	0	0	0	0	
24	0	0	0	0	
25	0	0	0	0	
26	0	0	0	0	
27	0	0	0	0	
28	0	0	0	0	
29	0	0	0	0	
30	0	0	0	0	

Observer's Name (print) Timothy J. Senger

Observer's Signature Timothy J. Senger 14 Dec 93

Organization TRC Environmental Corp.

Certified By EPA Region 1 5 Oct 93

Continued on YEO Form Number

TRC

Visible Emission Observation Form

Company Name BFI

Street Address 845 Burnett Road

City Chicopee State MA Zip 01020

Phone (key contact) (413) 592-8168 Source ID Number Stack #1

Process Equipment Landfill gas fired generator Operating Mode Full

Control Equipment Muffler Operating Mode Full/Normal

Describe Emission Point Muffler Vent (Horizontal)

Height Above Ground Level 73' Height Relative to Observer Start 17' End 17'

Distance from Observer Start 100' End 100' Direction from Observer Start NW End NW

Describe Emissions Start No Physical Char. End No Physical Char.

Emission Color Start None End None If Water Droplet Plume Attached ☐ Detached ☐

Point in the Plume at which Opacity was Determined Start End of outlet End End of outlet

Describe Plume Background Start Overcast White Sky End Overcast White Sky

Background Color Start White End White Sky Conditions Start Overcast End Overcast

Wind Speed Start 15mph End 15mph Wind Direction Start 0° N End 0° N

Ambient Temp Start 43°F End 42°F Wet Bulb Temp 35°F RH, Percent 50

Stack with Plume ☐ Sun ☒ Wind ☒

Source Layout Sketch

Draw North Arrow

Emission Point

Observer's Position

Sun Location Line

Additional Information Stack #1 Run #3
Sheet 1 of 2

Observation date 11 Dec 93 Start Time 1300 End Time 1330

MIN	SEC	0	15	30	45	Comments
1	0	0	0	0		
2	0	0	0	0		
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30	0	0	0	0		

Observer's Name (print) Timothy J. Senger

Observer's Signature Timothy J. Senger 14 Dec 93

Organization TRC Environmental Corp.

Certified By EPA Region 1 5 Oct 93

Continued on VEO Form Number

TRC

Visible Emission Observation Form

Company Name <u>BFI</u>		
Street Address <u>845 Burnett Road</u>		
City <u>Chicopee</u>	State <u>MA</u>	Zip <u>01020</u>
Phone (key contact) <u>(413) 592-8168</u>	Source ID Number <u>Stack #1</u>	

Process Equipment <u>Landfill gas fired generator</u>	Operating Mode <u>Full</u>
Control Equipment <u>Muffler</u>	Operating Mode <u>Full/Normal</u>

Describe Emission Point <u>Muffler Vent (Horizontal)</u>	
Height Above Ground Level <u>23'</u>	Height Relative to Observer Start <u>17'</u> End <u>17'</u>
Distance from Observer Start <u>100'</u> End <u>100'</u>	Direction from Observer Start <u>NW</u> End <u>NW</u>

Describe Emissions Start <u>No Physical Char.</u> End <u>No Physical Char.</u>	
Emission Color Start <u>None</u> End <u>None</u>	If Water Droplet Plume Attached ☐ Detached ☐
Point in the Plume at which Opacity was Determined Start <u>End of outlet</u> End <u>End of outlet</u>	

Describe Plume Background Start <u>Overcast white sky</u> End <u>Overcast white sky</u>	
Background Color Start <u>White</u> End <u>White</u>	Sky Conditions Start <u>Overcast</u> End <u>Overcast</u>
Wind Speed Start <u>15mph</u> End <u>10mph</u>	Wind Direction Start <u>0° N</u> End <u>0° N</u>
Ambient Temp. Start <u>42°F</u> End <u>43°F</u>	Wet Bulb Temp Start <u>30°F</u>
	RH, Percent <u>50</u>

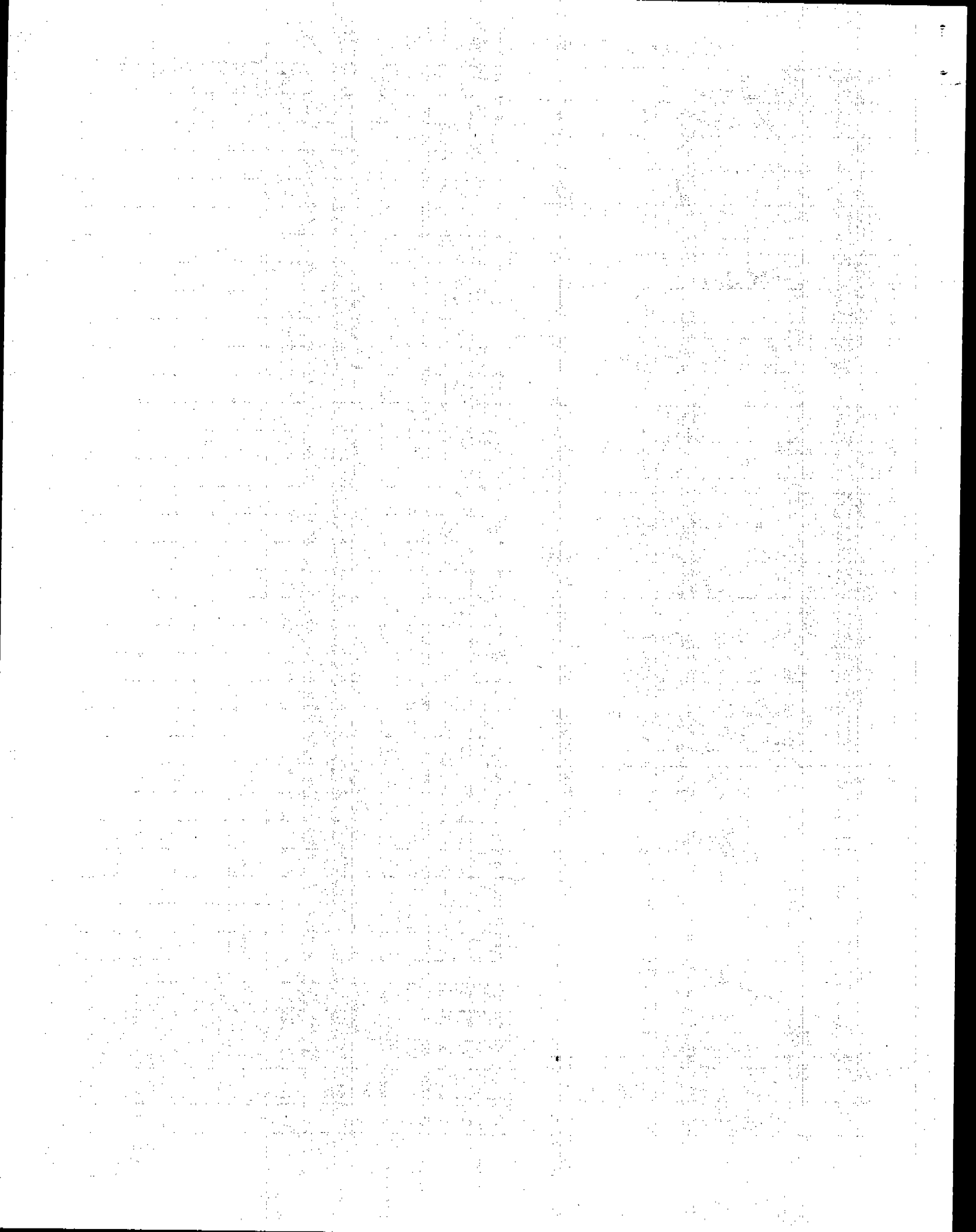
Stack with Plume	Source Layout Sketch	Draw North Arrow
Sun	Emission Point	
Wind	Observer's Position	
	Sun Location Line	

Additional Information <u>Stack #1 Run #3</u>
<u>Sheet 2 of 2</u>

Observation date <u>14 Dec 93</u>	Start Time <u>1330</u>	End Time <u>1400</u>			
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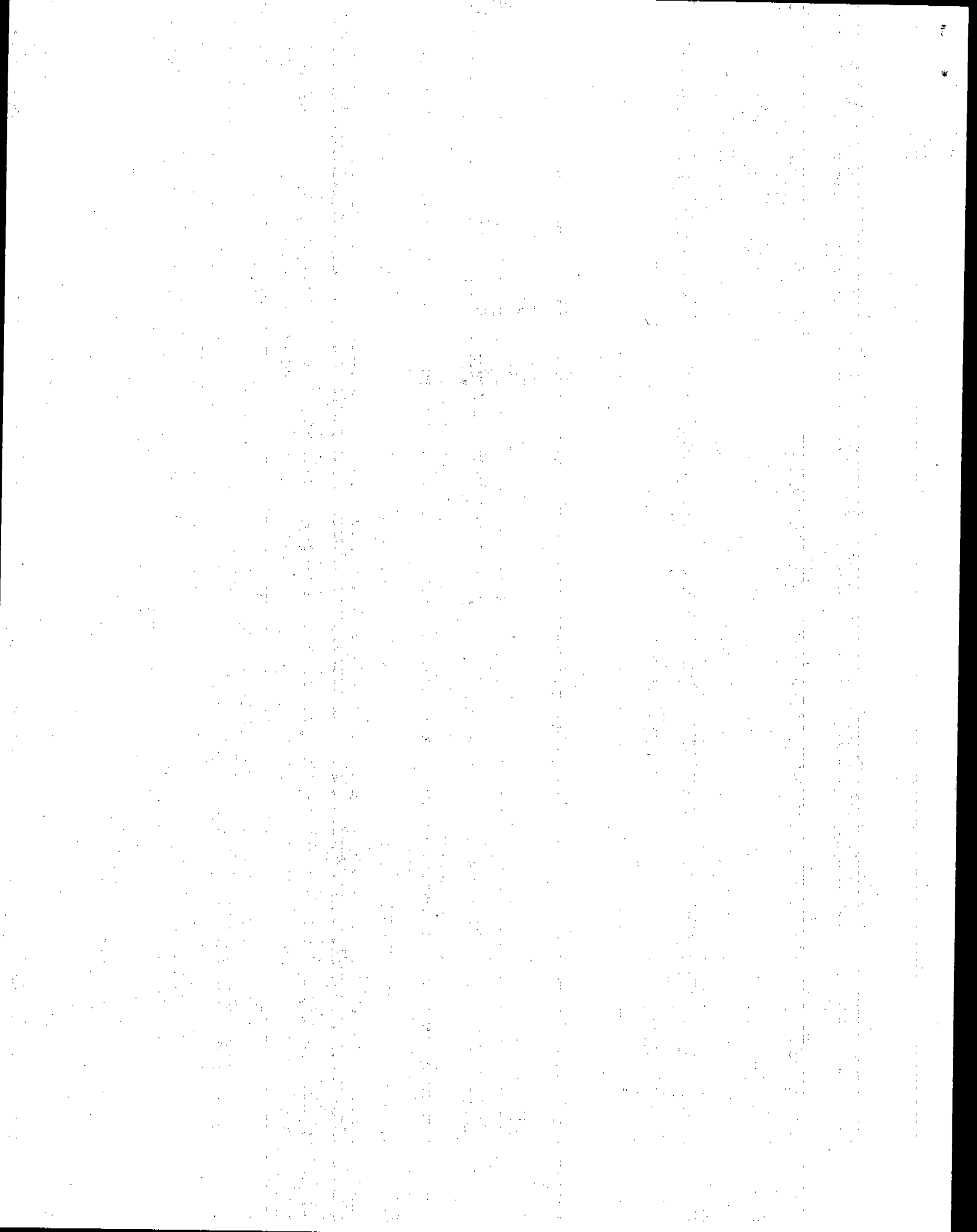
Observer's Name (print) <u>Timothy J. Senger</u>
Observer's Signature <u>Timothy J. Senger</u> <u>14 Dec 93</u>
Organization <u>TRC Environmental Corp.</u>
Certified By <u>EPA Region 1</u> <u>5 Oct 93</u>
Continued on VEO Form Number <u> </u>

TRC



APPENDIX E

FACILITY PROCESS DATA



A		B		C		D		E		F		G		H									
1	MAIN FUEL STATIC PSIG	MAIN FUEL DIFF. IN H2O	MAIN FUEL FLOW TEMP. ° F	MAIN FUEL FLOW CFM	MAIN FUEL FLOW MMBTU/HR	TOTAL FUEL FLOW MMBTU/HR	COMBINED GENERATOR KW	STATION AMBIENT ° F															
	10.9	18.10	78.0	706	22.178	22.954	3081	42.5															
2	PRECHAMBER FUEL PSIG	PRECHAMBER FUEL "H2O-DIFF."	PRECHAMBER FUEL ° F	PRECHAMBER FUEL FLOW CFM	PRECHAMBER FUEL FLOW MMBTU/HR	EXPORT HEAT RATE BTU/KW-HR	ENGINE HEAT RATE BTU/KW-HR	GEN SETS LOAD LEVELS															
	50.1	13.6	53.8	25	0.776	7749	7451																
3	STATION EXPORT KW	EXPORTED POWER KW-HR	STATION PARASITIC KW	PARASITIC POWER KW-HR	LANDFILL GAS BTU DRY	LANDFILL GAS BTU SAT'D	LANDFILL GAS S. GRAVITY	LANDFILL GAS COMPR'BLTY															
	2962	28396.94	121	1409.05	532.9	523.8	0.982	0.997															
4	STATION FUEL PROCESSING GRAPHIC	STATION ENGINE GENERATOR GRAPHIC	UNIT #1 ENGINE GENERATOR GRAPHIC	UNIT #2 ENGINE GENERATOR GRAPHICS	UNIT #3 ENGINE GENERATOR GRAPHICS	Unit #1 LOAD KW	Unit #2 LOAD KW	Unit #3 LOAD KW															
						1027.1	1021.8	1026.8															
5	LANDFILL SUCTION "HG"	LANDFILL SUCTION IN H2O	OUTPUT TO VFD PSIG	SETPOINT TO VFD PSIG	TOTAL FUEL FLOW/DAY MMBTU	ENGINE #1 HORSEPOWER HP	ENGINE #2 HORSEPOWER HP	ENGINE #3 HORSEPOWER HP															
	-0.5	-6.8	0.0	11.5	220.90	1449	1441	1448															
6	PLANT PROCESS GROUP	COMPRESSOR DISCHARGE PSIG	OUTPUT TO BYPASS	SETPOINT TO BYPASS	MAIN UTILITY BREAKER	UNIT#1 52A BREAKER	UNIT#2 52A BREAKER	UNIT#3 52A BREAKER															
		12.9	21.5	13.0	CLOSED	CLOSED	CLOSED	CLOSED															
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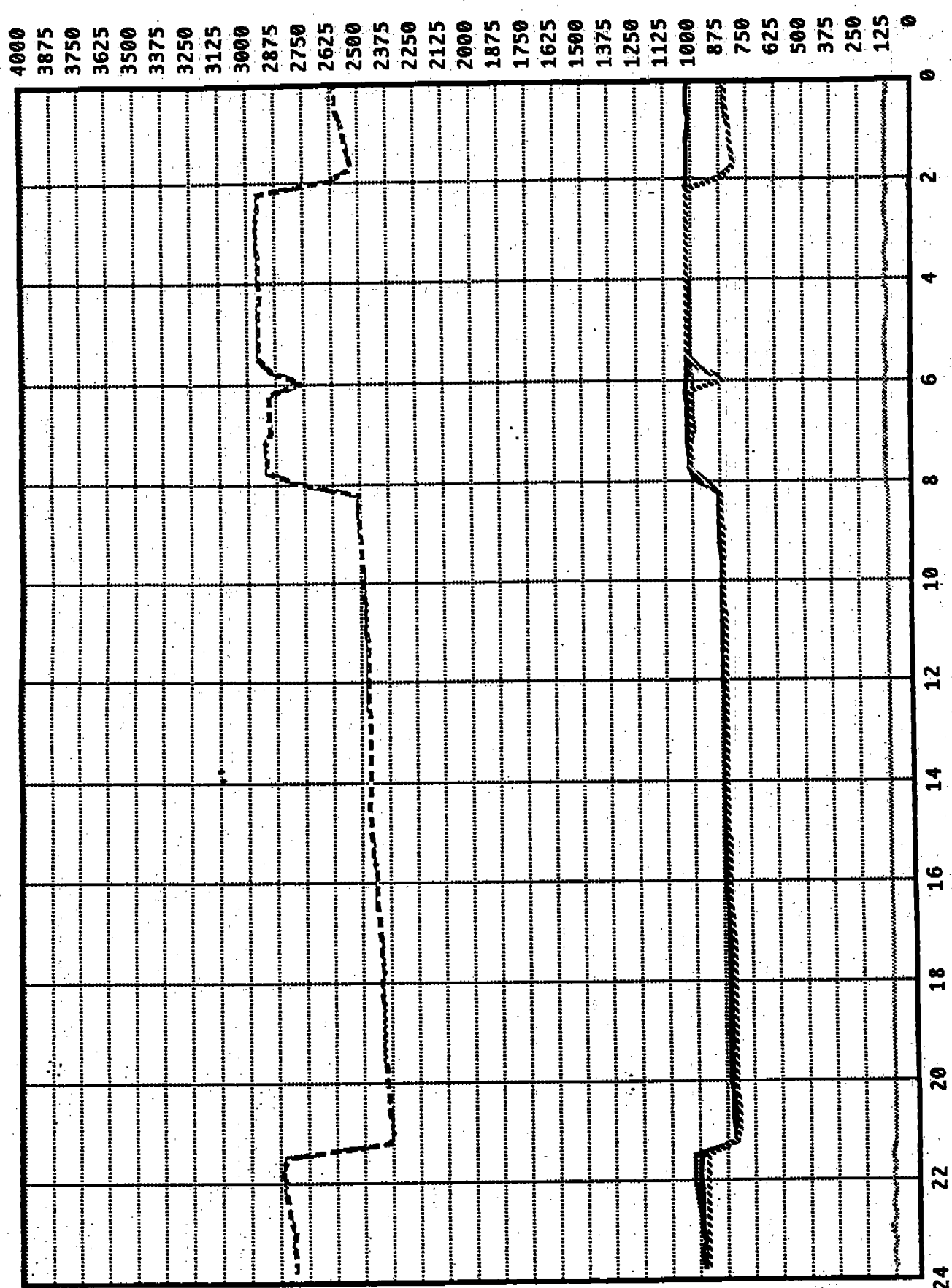
	A		B		C		D		E		F		G		H										
	MAIN FUEL STATIC PSIG	11.2	MAIN FUEL DIFF. IN H2O	14.70	MAIN FUEL FLOW TEMP. ° F	78.4	MAIN FUEL FLOW CFM	644	MAIN FUEL FLOW MMBTU/HR	20.275	TOTAL FUEL FLOW MMBTU/HR	21.080	COMBINED GENERATOR KW	2732	STATION AMBIENT ° F	45.5									
1	PRECHAMBER FUEL PSIG	41.0	PRECHAMBER FUEL "H2O-DIFF."	17.0	PRECHAMBER FUEL ° F	52.9	PRECHAMBER FUEL FLOW CFM	26	PRECHAMBER FUEL FLOW MMBTU/HR	0.804	EXPORT HEAT RATE BTU/KW-HR	7988	ENGINE HEAT RATE BTU/KW-HR	7717	GEN SETS LOAD LEVELS										
2	STATION EXPORT KW	2639	EXPORTED POWER KW-HR	45073.66	STATION PARASITIC KW	124	PARASITIC POWER KW-HR	2177.52	LANDFILL GAS BTU DRY	533.5	LANDFILL GAS BTU SAT'D	524.4	LANDFILL GAS S. GRAVITY	0.982	LANDFILL GAS COMPR'BLTY										
3	STATION FUEL PROCESSING GRAPHIC		STATION ENGINE GENERATOR GRAPHIC		UNIT #1 ENGINE GENERATOR GRAPHIC		UNIT #2 ENGINE GENERATOR GRAPHICS		UNIT #3 ENGINE GENERATOR GRAPHICS		Unit #1 LOAD kW		Unit #2 LOAD kW		Unit #3 LOAD kW										
4	LANDFILL SUCTION "HG"	-0.5	LANDFILL SUCTION IN H2O	-6.4	OUTPUT TO VFD PSIG	0.0	SETPOINT TO VFD PSIG	11.5	TOTAL FUEL FLOW/DAY MMBTU	347.48	ENGINE #1 HORSEPOWER HP	1021.5	ENGINE #2 HORSEPOWER HP	881.4	ENGINE #3 HORSEPOWER HP										
5	PLANT PROCESS GROUP		COMPRESSOR DISCHARGE PSIG	12.9	OUTPUT TO BYPASS	10.6	SETPOINT TO BYPASS	13.0	MAIN UTILITY BREAKER		UNIT #1 52A BREAKER		UNIT #2 52A BREAKER		UNIT #3 52A BREAKER										
6	Page	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	Scanning...			

Total load = 2758

APLP CHICOPEE POWER PLANT

Tue, Dec 14, 1993

4:47:18 PM



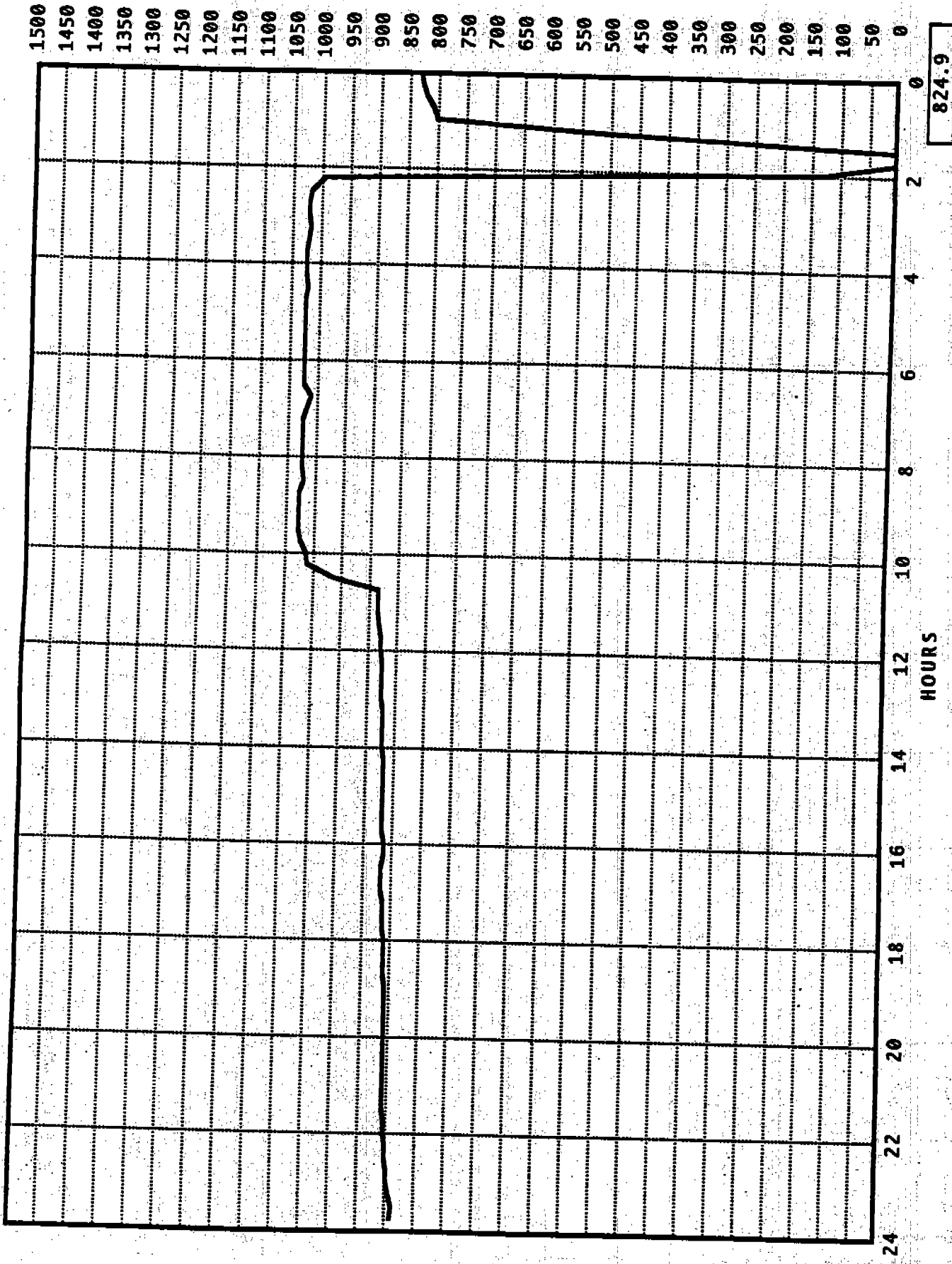
Unit #1
LOAD
kW

Unit #2
LOAD
kW

Unit #3
LOAD
kW

STATION
EXPORT
kW

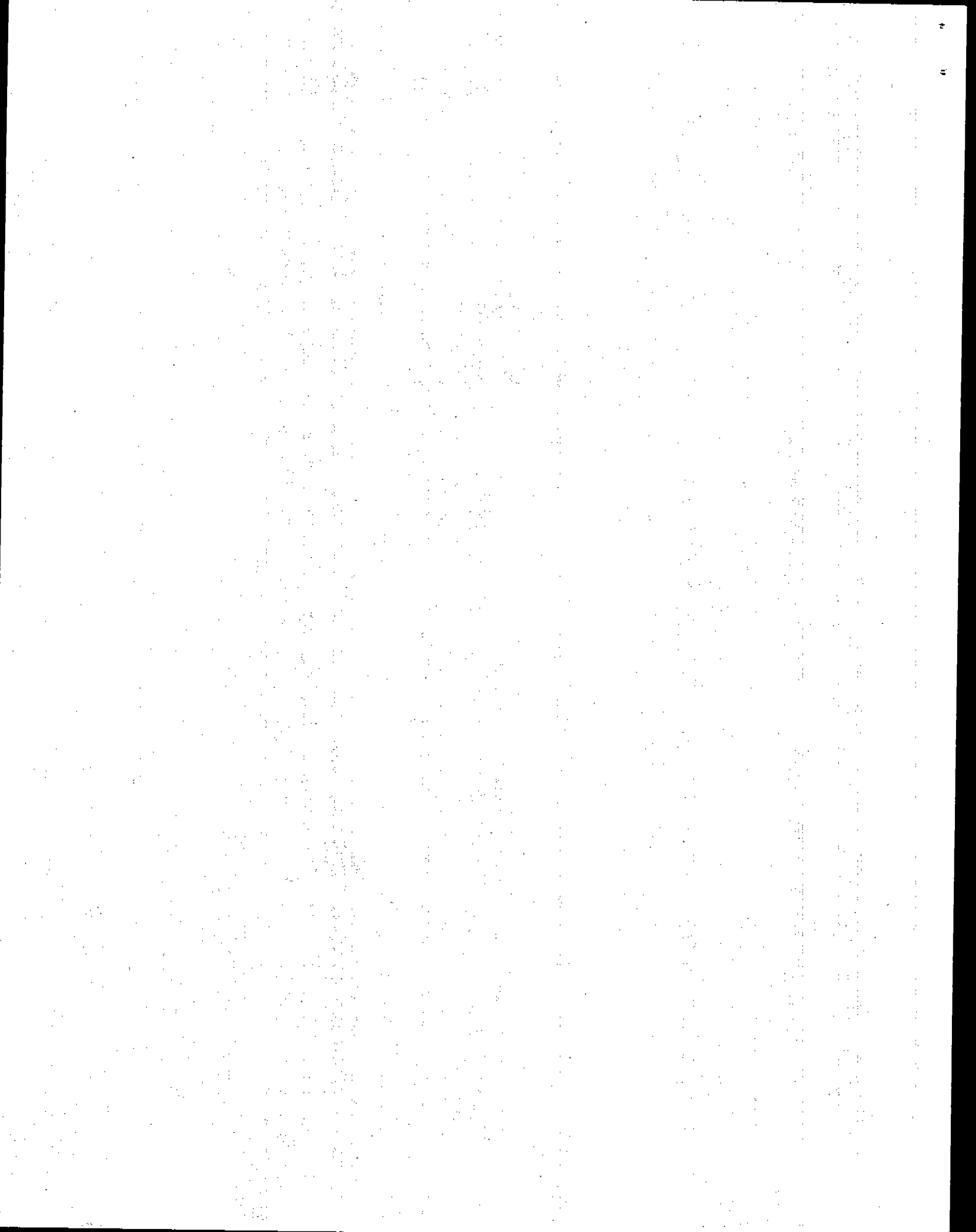
STATION
PARASITIC
kW



824.9

APPENDIX F

CALIBRATION SHEETS



Dry Gas Meter Calibration

Calibrated By Scott Tibbitts

Barometric Pressure, $P_b = 30.18$ in. Hg

Date 1/12/94

Meter Box No. 8130

Orifice manometer setting ΔH , in. H_2O	Gas volume wet test meter V_w , ft ³	Gas volume dry test meter V_d , ft ³	Temperature				Time Θ , °F	Y	$\Delta H\theta$	Deviation		
			Wet test Meter t_w , °F	Dry gas meter						Y	$\Delta H\theta$	
				Inlet t_{di} , °F	Outlet t_{do} , °F	Average t_d , °F						
0.5	5.67	6.013	67.3	87.9	84	85.95	15	.975	1.579	0.000	-0.062	
1.0	7.893	8.398	67.3	91	85	88	15	.974	1.935	-0.001	-0.006	
2.0	10.955	11.636	67.3	93.8	85	89.4	15	.976	2.009	0.001	+0.068	
Average									.975	1.941		

Calculations

Y	$\Delta H\theta$
$\frac{V_w P_b (t_d + 460)}{V_d (P_b + \frac{\Delta H}{13.6}) (t_w + 460)}$	$\frac{0.0317 \Delta H}{P_b (t_d + 460)} \left[\frac{(t_w + 460) \Theta}{V_w} \right]^2$

Y = Ratio of accuracy of wet test meter to dry test meter.
Tolerance = ± 0.01

$\Delta H\theta$ = Orifice pressure differential that gives 0.75 cfm of air
as 68° F and 29.92 inches of mercury, in. H_2O .
Tolerance = ± 0.15

METER BOX CALIBRATION WORKSHEET

Time Minutes	Inlet Temp.	Outlet Temp.	Meter Box Ser. # 8130	Date 1/12/41	
0	87	84	DGM Serial #	BAR Press (PB) 3.25	
2	88	84	ΔH (5) 1.0 2.0	Calibrated by 87	
4	88	84			
6	88	84	Final DGM 652.002	Final WTM 7480.555	
8	88	84	Initial DGM 675.989	Initial WTM 7874.845	
10	88	84	Net DGM 6.013	Net WTM 5.67	
12	88	84			
14	88	84	Vac. in. HG.	Average DGM Temperature 85.45 (54.45)	
15	88	84	4		
Avg.	87.9	84	$y = \frac{5.67 \times 30.18 \times 54.45}{6.013 \times (30.18 \times \frac{54.45}{13.6}) + 527.3} = 6.175$		
		(54.4)			
			$\Delta H = \frac{0.317 \times 5}{30.18 \times 54.4} \left[\frac{527.3 \times 15}{5.67} \right]^2 = 1.879$		
			Wet Test Meter Temperature	67.3 (527.3)	
			Total Time, minutes; seconds	15.0	

Calculations

Y	ΔH_0
$\frac{V_w P_b (t_d + 460)}{V_d (P_b + \frac{\Delta H}{13.6}) (t_w + 460)}$	$\frac{0.0317 \Delta H}{P_b (t_d + 460)} \left[\frac{(t_w + 460) e}{V_w} \right]^2$

METER BOX CALIBRATION WORKSHEET

Time Minutes	Inlet Temp.	Outlet Temp.	Meter Box Ser. # 5130	Date 1/12/94			
0	91	85	DGM Serial #	BAR Press (PB) 30.15			
2	91	85	ΔH .5 <u>1.0</u> 2.0	Calibrated by 87			
4	91	85					
6	91	85	Final DGM 674.214	Final WTM 78 73.175			
8	91	85	Initial DGM 665.816	Initial WTM 78 65.282			
10	91	85	Net DGM	Net WTM			
12	91	85					
14	91	85	Vac. in. HG. 4	Average DGM Temperature 88 (545)			
15	91	85					
Avg.	91	85	$Y = \frac{78.3 \times 30.15 \times 545}{8.398 \times (30.15 + 545)} = 1.174$				
		545					
			$\Delta H = \frac{0.0317}{30.15 + 545} \left[\frac{527.3 \times 15}{7.543} \right]^2 = 1.135$				
		Wet Test Meter Temperature					
		67.3 (527.3)					
		Total Time, minutes; seconds					
		15.0					

Calculations

Y	ΔH
$\frac{V_w P_b (t_d + 460)}{V_d \left(P_b + \frac{\Delta H}{13.6} \right) (t_w + 460)}$	$\frac{0.0317 \Delta H}{P_b (t_d + 460)} \left[\frac{(t_w + 460) \theta}{V_w} \right]^2$

Time Minutes	Inlet Temp.	Outlet Temp.	Meter Box Ser. # 8130	Date 1/12/94
0	92	85	DGM Serial #	BAR Press (PB) 30.18
2	92	85	ΔH .5 1.0 <u>(2.0)</u>	Calibrated by ST
4	93	85		
6	94	85	Final DGM 663.592	Final WTM 7853.48
8	94	85	Initial DGM 652.256	Initial WTM 7852.525
10	94	85	Net DGM 11.636	Net WTM 10.955
12	95	85		
14	95	85	Vac. in. HG. 4	Average DGM Temperature 84.4 (549.4)
15	95	85		
P.A.	63.8	55		$y = \frac{10.955 \times 30.18 \times 549.4}{11.636 \times (30.18 - \frac{2}{1.36}) + 527.3} = .476$
		54.5		
			$\Delta H = \frac{(63.8 \times 2)}{30.18 \times 54.5} \left[\frac{527.3 \pm 15}{10.955} \right]^2 = 2.009$	
			Wet Test Meter Temperature 67.3 (527.3)	
			Total Time, minutes; seconds	15.0

Y	ΔH°
$\frac{V_w P_b (t_d + 460)}{V_d \left(P_b + \frac{\Delta H}{13.6} \right) (t_w + 460)}$	$\frac{0.0317 \Delta H}{P_b (t_d + 460)} \left[\frac{(t_w + 460) e}{V_w} \right]^2$

Thermocouple Calibration Form

[illegible]

Signature of Person Performing Calibration

Calibration Date

Dry Gas Meter Calibration

Calibrated By S. T. Gbetta

Date 11/24/93

Barometric Pressure, P_b = 30.54 in. Hg

Meter Box No. 8130

Orifice nanometer setting ΔH , in. H_2O	Gas volume wet test meter V_w , ft ³	Gas volume dry test meter V_d , ft ³	Temperature				Time θ , °F	Y	ΔH_0	Deviation		
			Wet test Meter t_w , °F	Dry gas meter						Y	ΔH_0	
				Inlet t_{di} , °F	Outlet t_{do} , °F	Average t_d , °F						
7.5	5.755	6.057	64.2	83	78	80.5	15	.98	1.80	.00	.08	
10	7.93	8.31	64.2	84.8	77.1	80.9	15	.98	1.84	.00	.01	
0	11.087	11.582	64.2	85.9	74.8	80.3	15	.98	1.95	.00	.07	
Average									.98	1.85		

Calculations

Y	ΔH_0
$\frac{V_w P_b (t_d + 460)}{V_d (P_b + \frac{\Delta H}{13.6}) (t_w + 460)}$	$\frac{0.0317 \Delta H}{P_b (t_d + 460)} \left[\frac{(t_w + 460) \theta}{V_w} \right]^2$

Y = Ratio of accuracy of wet test meter to dry test meter.
Tolerance = ± 0.01

ΔH_0 = Orifice pressure differential that gives 0.75 cfm of air
as 68° F and 29.92 inches of mercury, in. H_2O .
Tolerance = ± 0.15

METER BOX CALIBRATION WORKSHEET

Time Minutes	Inlet Temp.	Outlet Temp.	Meter Box Ser. # 8130	Date 11/24
0	82	78	DGM Serial #	BAR Press (PB) 30.54
2	83	78	ΔH (5) 1.0 2.0	Calibrated by 87
4	83	78		
6	83	78	Final DGM 846.244	Final WTM 5909.580
8	83	78	Initial DGM 840.187	Initial WTM 5903.825
10	84	78	Net DGM	Net WTM
12	83	78		
14	83	78	Vac. in. HG.	Average DGM Temperature
15	83	78		
15	83	78	4	80.5 (540.5)
Avg.	83	78	$Y = \frac{(5.755)(30.54)(540.5)}{(6.057)(30.54)(524.2)} = .979$	
		538		
			$\Delta H = \frac{.0317(5)}{30.54(538)} \left[\frac{524.2(15)}{5.755} \right]^2 = 1.80$	
			Wet Test Meter Temperature 64.2 (524.2)	
			Total Time, minutes; seconds 15.0	

Calculations

Y	ΔH
$\frac{V_w P_b (t_d + 460)}{V_d (P_b + \frac{\Delta H}{13.6}) (t_w + 460)}$	$\frac{0.0317 \Delta H}{P_b(t_d + 460)} \left[\frac{(t_w + 460) e}{V_w} \right]^2$

METER BOX CALIBRATION WORKSHEET

Time Minutes	Inlet Temp.	Outlet Temp.	Meter Box Ser. # 8130	Date 11/24
0	82	76	DGM Serial #	BAR Press (PB) 30.54
2	84	77	ΔH .5 <u>1.0</u> 2.0	Calibrated by 87
4	85	77		
6	85	77	Final DGM 839.64	Final WTM 5903.314
8	85	77	Initial DGM 831.332	Initial WTM 5895.380
10	85	77	Net DGM 8.308	Net WTM 7.934
12	85	77		
14	86	78	Vac. in. HG. 4	Average DGM Temperature 80.94 (540.94)
15	86	78		
	84.78	77.1	$y = \frac{7.934 \times 30.54 \times 540.94}{8.308 \times (30.54 \times \frac{1}{13.6}) \times 524.2} = .983$	
		537.1		
			$\Delta H = \frac{.0317(1)}{30.54 \times 537.1} \left[\frac{524.2 \times 15}{7.934} \right]^2 = 1.898$	
			Wet Test Meter Temperature 64.2 (524.2)	
			Total Time, minutes; seconds 15.0	

Calculations

Y	ΔH_0
$\frac{V_w P_b (t_d + 460)}{V_d \left(P_b + \frac{\Delta H}{13.6} \right) (t_w + 460)}$	$\frac{0.0317 \Delta H}{P_b (t_d + 460)} \left[\frac{(t_w + 460) e}{V_w} \right]^2$

METER BOX CALIBRATION WORKSHEET

Time Minutes	Inlet Temp.	Outlet Temp.	Meter Box Ser. # 8130	Date 11/24	
0	81	73	DGM Serial #	BAR Press (PB) 30.54	
2	84	74	Δ H .5 1.0 <u>2.0</u>	Calibrated by 87	
4	85	74			
6	86	74	Final DGM 830.214	Final WTM 5894.316	
8	87	75	Initial DGM 818.632	Initial WTM 5883.229	
10	87	75	Net DGM	Net WTM	
12	87	76			
14	88	76	Vac. in. HG.	Average DGM Temperature	
15	88	76			
Avg.	85.89	74.75	$y = \frac{11.087 \times 30.54 \times 540.34}{11.542(30.54 + \frac{2}{13.6}) \times 524.2} = .982$		
		534.78			
			$\Delta H = \frac{.0317(2)}{30.54 \times 534.78} \left[\frac{524.2 \times 15}{11.087} \right]^2 = 1.953$		
			Wet Test Meter Temperature 64.2 (524.2)		
			Total Time, minutes; seconds 15.0		

Calculations

Y	ΔH ₂
$\frac{V_w P_b (t_d + 460)}{V_d (P_b + \frac{\Delta H}{13.6}) (t_w + 460)}$	$\frac{0.0317 \Delta H}{P_b (t_d + 460)} \left[\frac{(t_w + 460) \Theta}{V_w} \right]^2$

[illegible]

Signature of Person Performing Calibration

Calibration Date

