

PETRO CHEM ENVIRONMENTAL SERVICES, INC.

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Note: This is a reference cited in AP 42, *Compilation of Air Pollutant Emission Factors, Volume I Stationary Point and Area Sources*. AP42 is located on the EPA web site at www.epa.gov/ttn/chief/ap42/

The file name refers to the reference number, the AP42 chapter and section. The file name "ref02_c01s02.pdf" would mean the reference is from AP42 chapter 1 section 2. The reference may be from a previous version of the section and no longer cited. The primary source should always be checked.

ENGINEERING SOURCE TEST LOG

EACHTON CHEMICAL COMPANY
6055 13th Avenue
Commerce, Colorado 80020
303.733.1111

Atmospheric Emission Test Log

UNIVERSITY

STANDARD INDUSTRIAL CHEMICAL

TEST LOG

SECTION 1

DATE: 10/1/94

TESTER: J. L. HARRIS

TESTER: J. L. HARRIS

INSTRUCTIONS: PRINT OUT 107-107-107

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Ref #31 10/14/90
Tested for phenols
but none detected
air toxics incl
benzene
formaldehyde
Used heat flow
& fuel content
from 12/90 tests

SUMMARY OF RESULTS

COMPANY : PACIFIC ENERGY
 UNIT : OXNARD LANDFILL ENGINE #2
 DATE : 12-20-90
 REPORT : 62-372

DESTRUCTION REMOVAL EFFICIENCY OF HYDROCARBONS

OUTLET C1-C6+ TOTAL HYDROCARBON ANALYSIS

RUN #		C1-C6+		DRE
		INLET LB/HR	OUTLET LB/HR	% REDUCTION
#1		757.81	578.48	23.7
#2		757.81	452.24	40.3
#3		757.81	372.92	50.8

avg = 36.3

OUTLET C1-C5: EXCLUDES C6+

RUN #		C1-C5		DRE
		INLET LB/HR	OUTLET LB/HR	% REDUCTION
#1		757.81	137.07	81.9
#2		757.81	130.24	82.8
#3		757.81	129.52	82.9

avg = 82.5

INTRODUCTION

On December 20th, 1990, Petro-Chem Environmental Services (PCES) performed an engineering test for PACIFIC ENERGY SYSTEMS. The unit tested was at the Oxnard Landfill, Engine #2. Testing was to determine the destruction removal efficiency of hydrocarbons. The following parameters were tested using the following procedures:

<u>Parameter</u>	<u>Methods</u>	<u>#Tests/Engine</u>
Inlet hydrocarbon rate (lbs/hr)	Fuel Gas Analysis/Fuel Rate	2
Outlet hydrocarbon rate (lbs/hr)	Fuel gas Analysis/Fuel Rate EPA Method 18	3
%O ₂ , N ₂ , CO ₂	EPA Method 3 ORSAT Analysis	3
Removal Efficiency (%)	Mathematical Calculation	3

All testing was performed by Mr. Bob Martin of Petro-Chem Environmental Services. The fuel analysis was performed by Pacific Gas Technology of Bakersfield, CA.

DISCUSSION

DISCUSSION

The hydrocarbon data for Oxnard Landfill Engine #2 was reduced in two (2) ways.

1. The outlet C1-C6+ total hydrocarbons were analyzed for destruction removal efficiency.
2. Outlet C6+ was omitted from the analysis of DRE; assuming that the C6+ was a product of engine oil burn.
3. During Run #1 outlet of HC sample, a spark plug was changed.

INLET HYDROCARBON RATES

COMPANY : PACIFIC ENERGY
 UNIT : OXNARD LANDFILL ENGINE #2
 DATE : 12-20-90 LAB # 2048-2
 REPORT : 62-372

INLET - HYDROCARBONS

SCFM = 733.0

		ppm	lb/hr	ppm as CH4(as Methane)	lb/hr
Methane	(C1)	408700.0	757.810	408700.0	757.810
Ethane	(C2)	0.00	0.0000	0.00	0.00
Propane	(C3)	0.00	0.0000	0.00	0.00
Butane	(C4)	0.00	0.0000	0.00	0.00
Pentane	(C5)	0.00	0.0000	0.00	0.00
Hexane	(C6)	0.00	0.0000	0.00	0.00
Total		408700.0	757.810	408700.0	757.810

PACIFIC GAS TECHNOLOGY



4200 Easton Drive - Suite 5
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GAS ANALYSIS BY CHROMATOGRAPH

PETROCHEM ENVIRONMENTAL SERVICES
3207 Antonino Avenue
Bakersfield, CA 93388

Attention: Faythe Blythe

SAMPLED: DECEMBER 20, 1990

SUBMITTED: DECEMBER 28, 1990

REPORTED: DECEMBER 28, 1990

LAB # 2048-2

Sample ID : PACIFIC ENERGY
OXNARD LANDFILL
ENGINE #2, #8

CUSTOMER
NUMBER : 01208

CUSTOMER

JOB NUMBER: 62-372

ANALYZED GAS

	MOLE %	WT %	CHONS WT %
OXYGEN	4.43	4.98	CARBON 30.84
NITROGEN	22.53	22.19	HYDROGEN 5.79
CARBON DIOXIDE	32.17	49.78	OXYGEN 41.18
HYDROGEN	ND	0.00	NITROGEN 22.19
CARBON MONOXIDE	ND	0.00	SULFUR 0.00
		0.00	
METHANE	40.87	23.05	
ETHANE	ND	0.00	
PROPANE	ND	0.00	
iso-BUTANE	ND	0.00	
n-BUTANE	ND	0.00	
iso-PENTANE	ND	0.00	
n-PENTANE	ND	0.00	
HEXANE +	ND	0.00	

SPECIFIC GRAVITY * : 0.982

HYDROGEN SULFIDE : ppm
(Draeger)

* CALCULATED ACCORDING TO :

ASTM D-3588

TOTAL * DRY : 414

BTU/cu ft WET : 407

HYDROCARBON EMISSIONS TESTING
METHODS AND EQUATIONS

REF: EPA METHOD 18; FID ANALYSIS

SAMPLING PROCEDURES:

The sample was drawn via evacuated cannister through a stainless steel/teflon probe into a tedlar bag. Each sample bag was evacuated three (3) times, and then filled.

ANALYTICAL PROCEDURES:

The contents of the tedlar bag are analyzed by gas chromatography. The gas chromatograph is calibrated with an appropriate standard for each carbon #, before and after each set of samples are analyzed. The sample is speciated by carbon #-C1, C2, C3, C4, C5, and C6+ backflush.

SYMBOL IDENTIFICATION:

i = carbon #; i = 1 to 6+

s = refers to standard for that carbon #

Rx_i = response factor for C_i

MW = molecular weight - g/mole

DSCFM = Average volume flow rate of unit tested

EQUATIONS

$$Rx_i = \frac{ppm_{std}}{Area_s} \quad Rx_i = \frac{Area_{std}}{ppm_{std}}$$

$$Sample\ ppm_i = \frac{1}{Rx_i} \times Area_i$$

$$Sample\ ppm\ (as\ C_1) = Sample\ ppm \times \# \ of\ Carbons$$

$$\frac{lbs}{hr_i} = ppm_i \times MW_i \times DSCFM \times 1.581 \times 10^{-7}$$

$$Total\ non-methane\ \frac{lbs}{hr} = \sum_{i=2}^{6+} \frac{lbs}{hr_i}$$

Note 1: If $\frac{lbs}{hr}$ as methane is required, MW will equal 16.0
(MW of methane)

Note 2: # of carbons: ethane = 2; propane = 3; etc...

OUTLET HYDROCARBON RATES

42-381 50 SHEETS 5 SQUARE
42-382 100 SHEETS 5 SQUARE
42-389 200 SHEETS 5 SQUARE

Run 1	CL+	71, 193.42	ppm @ 3112 as CH ₄
2	CL+	55, 193.94	
3	CL+	44, 285.51	
Avg		56, 863.29	

$$\text{Aug } d_{scfm} = 5315.0 @ 9.1/102$$

$$= 5315 \left(\frac{20.9 - 3}{20.9 - 9.1} \right) = 8063 \text{ dscfm } @ 3\% \text{ } O_2$$

COMPANY: PACIFIC ENERGY
 UNIT : OXNARD LANDFILL ENGINE #2
 DATE : 12-20-90
 REPORT : 62-372

HYDROCARBON RESULTS

RUN No: 1
 GC RUN: 1 & 2 AVG
 DSCFM: 5315.0
 % O2: 9.1

Compound	Response Factor	Peak Area	Atten.	ppm	pm @3%O2
C1	664.73	6216705.0	1	9352.20	14186.81
C2	1082.03	0.0	1	0.00	0.00
C3	1682.95	123269.5	1	73.20	111.04
C4	2126.81	100082.5	1	47.10	71.45
C5	2771.48	290010.0	1	104.60	158.67
C6+	3546.62	21662000.0	1	6107.80	9265.22

	ppm	lb/hr	ppm as CH4	lb/hr (as CH4)	ppm @3%O2 as CH4
Methane (C1)	9352.2	125.739	9352.2	125.739	14186.81
Ethane (C2)	0.0	0.000	0.00	0.000	0.00
Propane (C3)	73.2	2.706	220	2.952	333.12
Butane (C4)	47.1	2.296	188	2.533	285.79
Pentane (C5)	104.6	6.328	523	7.032	793.36
Hexane (C6)	6107.8	441.386	36646.8	492.710	55591.33

Total	15684.9	578.45	46930.0	630.97	71190.42
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Total (non methane)	6332.70	452.72	37577.8	505.23	57003.61
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COMPANY: PACIFIC ENERGY
UNIT : OXNARD LANDFILL ENGINE #2
DATE : 12-20-90
REPORT : 62-372

HYDROCARBON RESULTS

RUN No: 2
GC RUN: 1 & 2 AVG
DSCFM : 5315.0
% O2 : 9.1

Compound	Response Factor	Peak Area	Atten.	ppm	pm @3%O2
C1	664.73	6130355.0	1	9222.3	13989.76
C2	1082.03	0.0	1	0.0	0.00
C3	1682.95	78666.0	1	46.7	70.84
C4	2126.81	33280.5	1	15.6	23.66
C5	2771.48	92357.0	1	33.3	50.51
C6+	3546.62	15802500.0	1	4455.7	6759.07

		ppm	lb/hr	ppm as CH4	lb/hr (as CH4)	ppm @3%O2 as CH4
Methane	(C1)	9222.3	125.739	9222.3	123.992	13989.76
Ethane	(C2)	0	0.000	0.0	0.000	0.00
Propane	(C3)	46.7	1.727	140.1	1.884	212.52
Butane	(C4)	15.6	0.760	62.4	0.839	94.66
Pentane	(C5)	33.3	2.015	166.5	2.239	252.57
Hexane	(C6)	4455.7	321.995	26734.2	359.437	40554.42
Total		13773.60	452.24	36325.50	488.39	55103.94

Total
(non methane) 4551.30 326.50 27103.20 364.40 41114.18

COMPANY: PACIFIC ENERGY
 UNIT : OXNARD LANDFILL ENGINE #2
 DATE : 12-20-90
 REPORT : 62-372

HYDROCARBON RESULTS

RUN No: 3
 GC RUN: 1 & 2 AVG
 DSCFM : 5315.0
 % O2 : 9.1

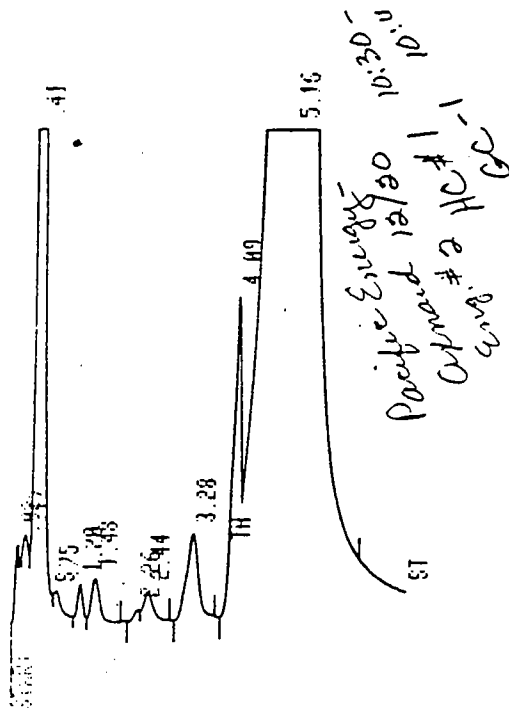
Compound	Response Factor	Peak Area	Atten.	ppm	pm @3%O2
C1	664.73	5766355.0	1	8674.70	13159.08
C2	1082.03	0.0	1	0.00	0.00
C3	1682.95	45400.5	1	27.00	40.96
C4	2126.81	43588.5	1	20.50	31.10
C5	2771.48	81688.0	1	29.50	44.75
C6+	3546.62	11945350.0	1	3368.10	5109.24

		ppm	lb/hr	ppm @3%O2
		ppm	lb/hr	as CH4
Methane (C1)	8674.7	125.739	8674.7	116.63
Ethane (C2)	0.0	0.000	0.0	0.00
Propane (C3)	27.0	0.998	81.0	1.09
Butane (C4)	20.5	0.999	82.0	1.10
Pentane (C5)	29.5	1.785	147.5	1.98
Hexane (C6)	3368.1	243.399	20208.6	271.70

Total	12119.80	372.92	29193.8	392.51	44285.51
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Total (non methane)	3445.10	247.18	20519.1	275.88	31126.43
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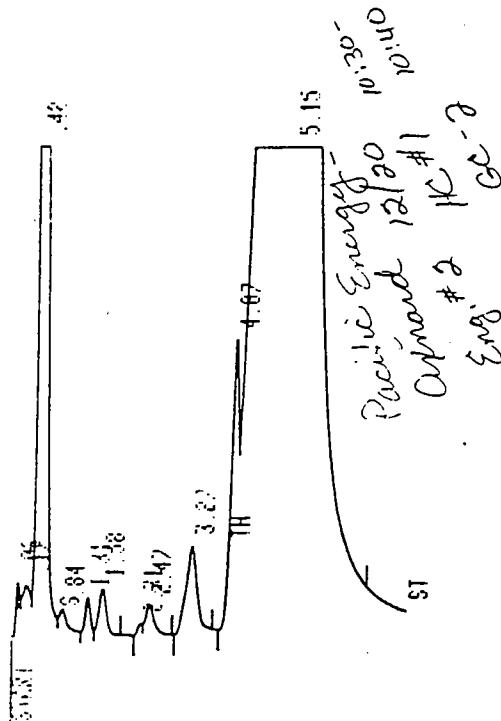
HYDROCARBONS RUN 1



RUN # 909 DEC/27/90 11:39:04

AREA%	RT	AREA TYPE	AR/HT	AREA%
0.02	0.975	10291-D BP	0.039	0.040
0.17	1.48	45389 PH	0.106	0.176
0.41	2.44	6095600 SHS	0.108	23.564
0.75	3.28	0-D-BP	0.000	0.000
1.48	4.49	46968-D-PV	0.102	0.102
2.26	5.16	88029 PB	0.156	3.340
2.44		19339 PV	0.124	0.075
3.28		76857 VB	0.196	0.297
4.09		282550 PB	0.244	1.092
5.16		653640 PV	0.147	2.327
1.8550E+07		VB	0.771	71.708

TOTAL AREA= 2.5868E+07
MUL FACTOR= 1.0000E+00

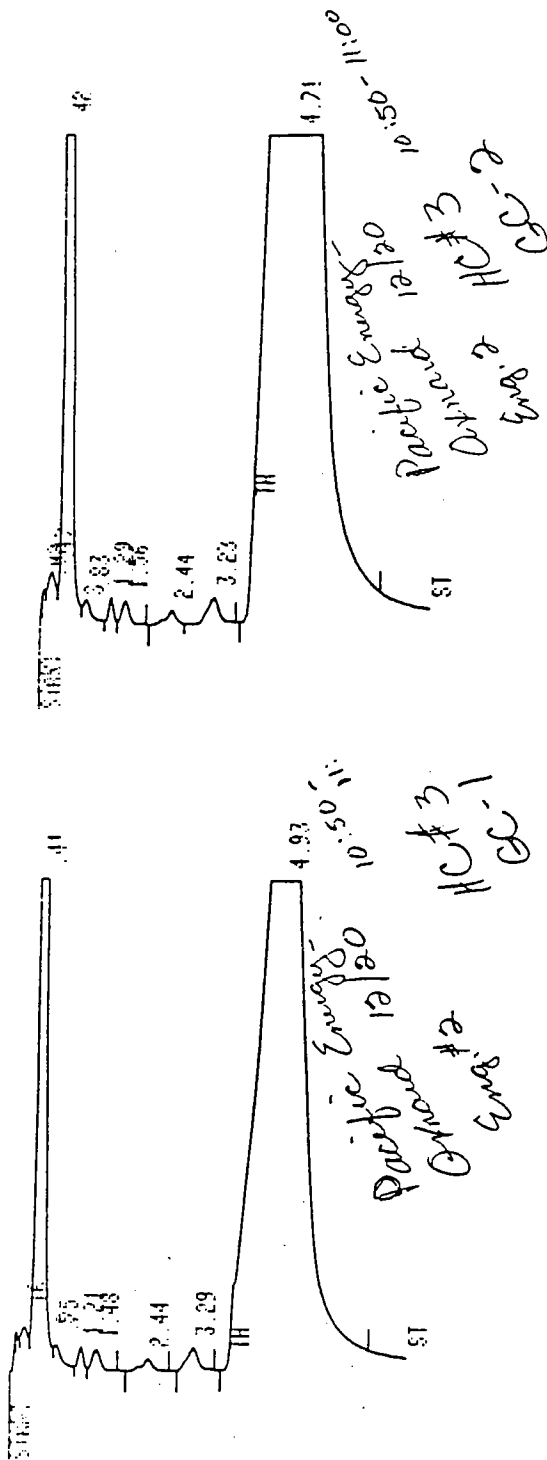


RUN # 912 DEC/27/90 13:19:14

AREA%	RT	AREA TYPE	AR/HT	AREA%
0.02	0.84	13432-D BY	0.044	0.042
0.17	1.38	31404 VH	0.120	0.097
0.42	2.47	6391800 SHS	0.113	19.724
0.84	3.23	12240-D BP	0.070	0.038
1.31	4.07	53500 PV	0.105	0.165
1.58	5.15	105010 VB	0.159	0.324
2.31		18364 BY	0.102	0.057
2.47		85605 VB	0.193	0.264
3.27		297470 PB	0.240	0.918
4.07		624030 PV	0.151	1.926
5.15		2.4774E+07 VB	0.891	76.447

TOTAL AREA= 3.2407E+07
MUL FACTOR= 1.0000E+00

HYDROCARBONS RUN 3



RUN # 916 DEC/27/90 14:58:59

AREA%	RT	AREA TYPE	AR/HT	AREA%
0.16	1.21	PH	0.112	0.157
0.41	1.48	SHB	0.105	37.760
0.75	2.44	0-0-BP	0.080	0.000
1.21	3.29	PF	0.105	0.215
2.143	4.93	PB	0.158	0.305
2.44		B8	0.237	0.279
3.29		PB	0.245	0.534
4.93		PB	0.879	60.751

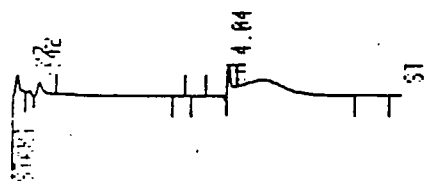
TOTAL AREA= 1.4371E+07
MUL FACTOR= 1.0000E+00

RUN # 917 DEC/27/90 15:30:08

AREA%	RT	AREA TYPE	AR/HT	AREA%
0.02	0.83	BV	0.054	0.064
0.17	1.42	VH	0.165	0.375
0.42	2.44	SHB	0.111	28.469
0.83	3.23	0-BP	0.052	0.035
1.29	4.71	D-PV	0.100	0.162
1.56		VB	0.149	0.217
2.44		PF	0.234	0.217
3.23		PB	0.244	0.401
4.71		PB	0.893	70.060

TOTAL AREA= 2.1638E+07
MUL FACTOR= 1.0000E+00

HYDROCARBONS He BLANK



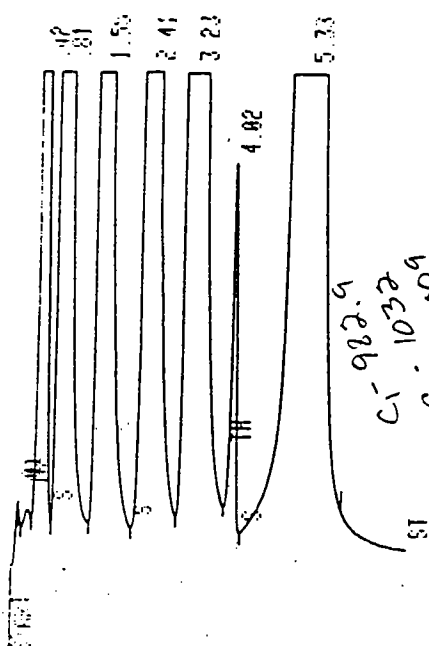
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RUN # 924 DEC/27/98 17:39:14

AREA%	RT	AREA	TYPE	AR/HT	AREN%
0.83	0.83	5829	D-BP	0.093	0.322
0.42	0.42	2695	PB	0.137	44.754
4.84	4.84	28295	D-PB	0.070	46.909

TOTAL AREA= 69319
MUL FACTOR= 1.0000E+00

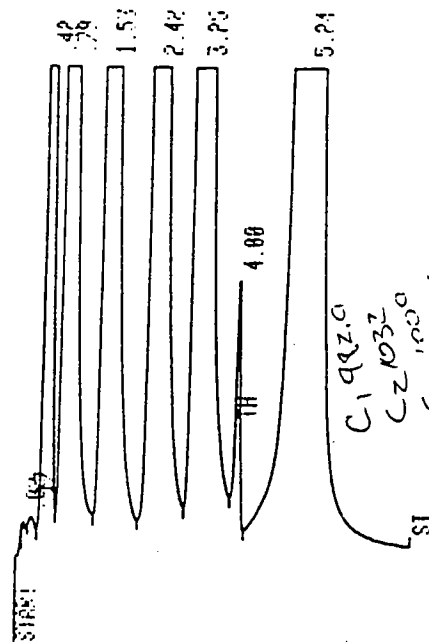
HYDROCARBONS INITIAL/FINAL



RUN # 910 DEC/27/90 12:00:41

AREA%	RT	AREA TYPE	AR/HT	AREA%
0.01	0.81	12678 D BP	0.041	0.013
0.18	0.81	PH	0.105	0.025
0.42	0.81	SHB	0.107	0.070
0.01	1.53	1.0833E+07	0.147	11.294
1.55	1.53	1.5519E+07	0.160	16.181
2.41	1.53	1.9725E+07	0.167	20.566
3.23	2.2083E+07	SHB	0.204	23.025
4.02	4.02	447450 DTB8	0.088	0.467
5.33	2.1638E+07	BB	0.384	22.560

TOTAL AREA= 9.5910E+07
MUL FACTOR= 1.0000E+00



RUN # 919 DEC/27/90 16:21:01

AREA%	RT	AREA TYPE	AR/HT	AREA%
0.02	0.81	12794 D BV	0.058	0.013
0.17	0.81	VH	0.154	0.042
0.42	0.81	5146300 SHH	0.103	5.296
0.79	1.1123E+07	SHH	0.150	11.445
1.53	1.5933E+07	SHH	0.165	16.396
2.42	2.0154E+07	SHH	0.173	20.739
3.25	2.2504E+07	ISHP	0.206	23.157
4.00	287730 DTB8	0.086	0.086	0.296
5.24	2.1973E+07	TPV	0.375	22.611

TOTAL AREA= 9.7179E+07
MUL FACTOR= 1.0000E+00

HYDROCARBON EMISSIONS TESTING
METHODS AND EQUATIONS

REF: EPA METHOD 18; FID ANALYSIS

SAMPLING PROCEDURES:

The sample was drawn via evacuated cannister through a stainless steel/teflon probe into a tedlar bag. Each sample bag was evacuated three (3) times, and then filled.

ANALYTICAL PROCEDURES:

The contents of the tedlar bag are analyzed by gas chromatography. The gas chromatograph is calibrated with an appropriate standard for each carbon #, before and after each set of samples are analyzed. The sample is speciated by carbon #-C1, C2, C3, C4, C5, and C6+ backflush.

SYMBOL IDENTIFICATION:

i = carbon #; i = 1 to 6+

s = refers to standard for that carbon #

Rx_i = response factor for C_i

MW = molecular weight - g/mole

DSCFM = Average volume flow rate of unit tested

EQUATIONS

$$Rx_i = \frac{ppm_{std}}{Area_s} \quad Rx_i = \frac{Area_{std}}{ppm_{std}}$$

$$Sample\ ppm_i = \frac{1}{Rx_i} \times Area_i$$

$$Sample\ ppm\ (as\ C_1) = Sample\ ppm \times \#\ of\ Carbons$$

$$\frac{lbs}{hr_i} = ppm_i \times MW_i \times DSCFM \times 1.581 \times 10^{-7}$$

$$Total\ non-methane\ \frac{lbs}{hr} = \sum_2^{6+} \frac{lbs}{hr_i}$$

Note 1: If $\frac{lbs}{hr}$ as methane is required, MW will equal 16.0

(MW of methane)

Note 2: # of carbons: ethane = 2; propane = 3; etc...

FUEL ANALYSIS

COMPANY: PACIFIC ENERGY
UNIT : OXNARD LANDFILL ENGINE #2
DATE : 12-20-90
REPORT : 62-372

DSCFM CALCULATIONS

SCFM = 733.0

FOLLOWING VALUES FOR GROSS MMBTU/CF AND 'F' FACTOR @ 60' F
TAKEN FROM 'EPA F-FACTOR FOR FUEL GAS' SHEET
LAB #2048-2

AVERAGED % O2 TAKEN FROM ORSAT ANALYSIS

0.000413 = MMBtu/CF % O2 = 9.1
9920.553 = DSCF/MMBTU

DSCF/MIN= 733.0 SCF/MIN *0.000413 MMBTU/CF*9920.5 DSCF/MMBTU

=3000.8 DSCF/MIN @ 0 % O2

DSCFM @ 9.1 % O2 = 3000.8 DSCF/MIN* (20.9/ (20.9 - 9.10

= 5315.00 DSCFM @ 9.1 % O2
=====

COMPANY: PACIFIC ENERGY
 UNIT : OXNARD LANDFILL ENGINE #2
 DATE : 12-20-90
 REPORT : 62-372

PACIFIC GAS: #2048-2

EPA "F" FACTOR FOR NATURAL GAS

FUEL COMPONENT	C	H	EXPANSION FACTOR	COMPONENT MOLE %	EXHAUST DSCF (0)/ SCF FUEL
-----	--	--	-----	-----	-----
METHANE	1	4	8.57	40.87	3.502559
ETHANE	2	6	15.25	0	0
PROPANE	3	8	21.92	0	0
(ISO-BUTANE)	4	10	28.6	0	0
NORM-BUTANE	4	10	28.6	0	0
(ISO-PENTANE)	5	12	35.28	0	0
NORM-PENTANE	5	12	35.28	0	0
HEXANE +	6	14	41.95	0	0
AIR (N2+O2)	--	--	1	26.96	0.2696
CO2	--	--	1	32.17	0.3217
H2S	--	--	6.68	0	0
				-----	-----
			TOTAL	100.00	4.093859

4.093859	DSCF EXHAUST PER SCF OF FUEL GAS AT ZERO % OXYGEN

371.5491	NET BTU/SCF OF FUEL GAS

412.6643	GROSS BTU/SCF OF FUEL GAS

9920.553	DSCF/MMBTU (EPA "F" FACTOR @ 60°F & ZERO % OXYGEN)

10071.62	DSCF/MMBTU (EPA "F" FACTOR @ 68°F & ZERO % OXYGEN)

PACIFIC GAS TECHNOLOGY



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GAS ANALYSIS BY CHROMATOGRAPH

PETROCHEM ENVIRONMENTAL SERVICES
3207 Antonino Avenue
Bakersfield, CA 93388

SAMPLED: DECEMBER 20, 1990

SUBMITTED: DECEMBER 28, 1990

Attention: Faythe Blythe

REPORTED: DECEMBER 28, 1990

LAB # 2048-2

Sample ID : PACIFIC ENERGY
OXNARD LANDFILL
ENGINE #2, =8

CUSTOMER
NUMBER : 01208

CUSTOMER

JOB NUMBER: 62-372

ANALYZED GAS

MOLE %

WT %

CHONS WT %

OXYGEN	4.43	4.98	CARBON	30.84
NITROGEN	22.53	22.19	HYDROGEN	5.79
CARBON DIOXIDE	32.17	49.78	OXYGEN	41.18
HYDROGEN	ND	0.00	NITROGEN	22.19
CARBON MONOXIDE	ND	0.00	SULFUR	0.00
		0.00		
METHANE	40.87	23.05		
ETHANE	ND	0.00		
PROPANE	ND	0.00		
iso-BUTANE	ND	0.00		
n-BUTANE	ND	0.00		
iso-PENTANE	ND	0.00		
n-PENTANE	ND	0.00		
HEXANE +	ND	0.00		

SPECIFIC GRAVITY * : 0.982

* CALCULATED ACCORDING TO :

HYDROGEN SULFIDE : ppm
(Draeger)

ASTM D-3588

TOTAL * DRY : 414
BTU/cu ft

WET : 407

PACIFIC GAS TECHNOLOGY



4200 Easton Drive - Suite 5
Bakersfield, California 93309
805/324-1317
Fax: 805/324-2746

GAS ANALYSIS BY CHROMATOGRAPH

PETROCHEM ENVIRONMENTAL SERVICES
3207 Antonino Avenue
Bakersfield, CA 93388

SAMPLED: DECEMBER 21, 1990

SUBMITTED: DECEMBER 28, 1990

Attention: Faythe Blythe

REPORTED: DECEMBER 28, 1990

LAB = 2048

Sample ID : PACIFIC ENERGY
OXNARD LANDFILL
ENGINE #2, #7

CUSTOMER
NUMBER : 01208

CUSTOMER
JOB NUMBER: 62-372

ANALYZED GAS

MOLE %

WT %

CHONS WT %

OXYGEN	11.18	12.32	CARBON	17.63
NITROGEN	46.20	44.58	HYDROGEN	3.10
CARBON DIOXIDE	20.30	30.77	OXYGEN	34.70
HYDROGEN	ND	0.00	NITROGEN	44.58
CARBON MONOXIDE	ND	0.00	SULFUR	0.00
METHANE	22.32	12.33		
ETHANE	ND	0.00		
PROPANE	ND	0.00		
iso-BUTANE	ND	0.00		
n-BUTANE	ND	0.00		
iso-PENTANE	ND	0.00		
n-PENTANE	ND	0.00		
HEXANE +	ND	0.00		

SPECIFIC GRAVITY * : 1.002

HYDROGEN SULFIDE : ppm
(Draeger)

* CALCULATED ACCORDING TO :

ASTM D-3583

TOTAL * DRY : 226

BTU/cu ft

WET : 222

F-FACTOR FOR GASEOUS FUELS

Ref: 1) Code of Federal Regulations 40 CFR 60.45
2) Handbook of Chemistry and Physics; CRC Press

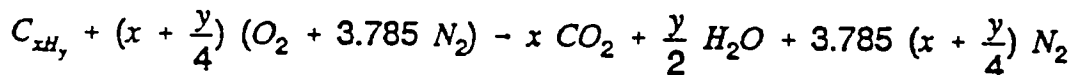
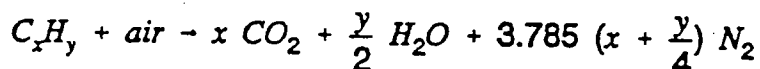
The F-Factor is the ratio of the total exhaust volume (DSCF°) produced by the stoichiometric combustion of 1 SCF of the gaseous fuel and the Btu content of the same 1 SCF of gaseous fuel.

$$\text{EPA F Factor} = F \frac{\text{DSCF}^\circ}{\text{MMBtu}} = 10^6 \times \frac{\frac{\text{DSCF}^\circ}{\text{SCF fuel}}}{\frac{\text{Btu}}{\text{SCF fuel}}}$$

STOICHIOMETRIC COMBUSTION OF HYDROCARBONS:

The exhaust volume concentration of each fuel gas component is determined by the general equation for the stoichiometric combustion of a gaseous hydrocarbon.

C_xH_y in air:



Therefore, for each mole (or standard cubic foot) of each fuel gas component C_xH_y , there will be:

$$1) \ x + \frac{y}{2} + 3.785 \left(x + \frac{y}{4}\right) \text{ moles (or SCF) of "wet" exhaust flow}$$

$$2) \ x + 3.785 \left(x + \frac{y}{4}\right) \text{ moles (or DSCF) of "dry" exhaust flow}$$

OR

1 SCF of C_xH_y produces $4.785x + 0.946y$ DSCF° flue gas

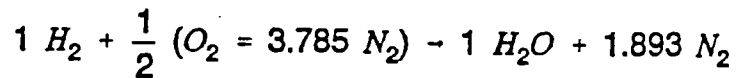
where: x = # of carbon atoms in component C_xH_y
 y = # of hydrogen atoms in component C_xH_y

If non-combustible components such as N_2 , O_2 , or CO_2 are present in the gaseous fuel, these will not participate in the combustion process.

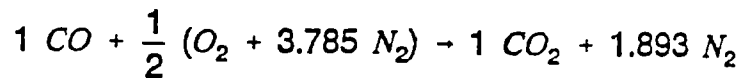
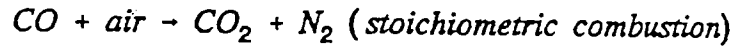
1 SCF Non-combustible component produces 1 SCF° flue gas.

STOICHIOMETRIC COMBUSTION OF HYDROCARBONS (con't)...

Hydrogen (H_2) combustion proceeds according to the reaction:



Carbon Monoxide (CO) combustion in air proceeds according to the reaction:



1 SCF CO produces 2.893 DSCF^o flue gas

The total exhaust gas volume at stoichiometric combustion (zero % excess O_2) is the summation of the individual component's contribution. The actual total exhaust gas volume is greater and depends on the % O_2 in the exhaust gas.

$$\text{Actual DSCF} = \text{DSCF}^o \text{ (@ stoichiometric combustion)} \times \frac{20.9}{20.9 - \% O_2 \text{ in exhaust gas}}$$

BTU HEATING CONTENT OF GASEOUS FUELS:

The Btu/SCF of the gaseous fuel is determined either by actual measurement of a sample combustion in a calorimeter or from a summation of the known heating value of the components multiplied by the mole fraction of the components.

ORSAT ANALYSIS



PETRO
CHEM
ENVIRONMENTAL
SERVICES

Client: PACIFIC ENERGY - Oxnard.
Date : 12-20-90
Unit :
Job # :

ORSAT ANALYSIS
%O₂, CO₂, N₂

Run #	% O ₂	% CO ₂	% N ₂
SAMPLE # 4	9.6	9.9	
SAMPLE # 5	8.6	10.1	
average	9.1	10.0	

