

Arizona St.

LFG EFD

AP42

Arizona St (Baird Park) Landfill

SURELITE FLARE

Note: This is a reference cited in AP 42, Compilation of Air Pollutant Emission Factors, Volume I Stationary Point and Area Sources. AP42 is located on the EPA web site at www.epa.gov/ttn/chief/ap42/

The file name refers to the reference number, the AP42 chapter and section. The file name "ref02_c01s02.pdf" would mean the reference is from AP42 chapter 1 section 2. The reference may be from a previous version of the section and no longer cited. The primary source should always be checked.

Data Qual = A.

November 25, 1992

TO: Michael R. Lake, Chief
Engineering Division

FROM: Dave Byrnes, Associate Toxics Engineer
Archi dela Cruz, Junior Toxics Engineer

EMISSION FACTORS FOR LANDFILL GAS FLARES

The San Diego Air Pollution Control District (District) contracted the South Coast Environmental Company (SCEC) to source test the Arizona Street and Bell Junior High School landfill gas flares. The sites were source tested for SO_x, NO_x, CO, TOG/ROG, particulates, and speciated toxic organic gases between March 30 and April 7, 1992.

The source test results of SCEC have been reviewed and approved by the District Monitoring and Technical Services Section (M&TS). District Toxics Engineering Section has generated the following emission factors for landfill gas flares using the M&TS approved source test reports. The emission factors are presented below in units of lbs of contaminant per million BTU.

Emission Factors for Landfill Gas Flares (lbs contaminant/mm BTU).

Contaminant	Arizona	Bell	Average	Recommended*	SCAQMD
SO _x	0.0077	0.0105	0.0091	0.01	0.001
NO _x	0.0825	0.0562	0.0694	0.10	0.05
CO	<0.0170	<0.0181	<0.0176	0.02	0.19
Particulates	0.0106	0.0207	0.0157	0.02	0.07
ROG**				0.06	0.42

* Recommended for permit processing.

** Inlet concentrations of 0.2 and a conservative destruction efficiency of 70% will be used for the purposes of permit processing.

ENGINEERING'S METHODOLOGY.

Both energy and mass balance were performed to verify the source test report information approved by M&TS. A carbon balance was used to determine the landfill gas flow at the inlet. A hydrogen balance was used to verify the methane content of the inlet landfill gas. Data from Arizona Run #3 and Bell Run #1 were determined to be acceptable after adjustment of the outlet stack temperatures, landfill gas inlet flow rates, and inlet methane concentrations.

An Excel spreadsheet was developed to calculate the energy at the inlet and at the outlet of the flare, the heat of combustion of the landfill gas, and the heat loss by the flare. Test results were adjusted to develop more accurate operating parameters. These operating parameters were verified by inspecting the heat loss as a percent of the total heat output.

Table 1 lists the key operating parameters that were used to produce reasonable energy balances and to determine the landfill emission factors.

Table 1. Flare Operating Parameters.

PARAMETERS	ARIZONA	BELL
Stack Temperature	2110°R	2010°R
Inlet Flow of Landfill Gas	242 cfm	316 cfm
Methane Content at Inlet	60%	55%

STACK TEMPERATURE CORRECTIONS.

It was discovered that SCEC's temperature readings may have been taken improperly and the temperature probe may have been calibrated incorrectly. At Arizona Street, M&TS noticed the SCEC did not allow the temperature probe to reach equilibrium after reinserting the probe into the next port or sampling location. M&TS corrected for this incorrect measurement technique and approved a temperature value of 1903°R. No correction was made by M&TS for the possible calibration error. The thermocouple installed in the site flare displayed an average temperature of 2110°R. A difference of 207° is observed between the two temperature probes.

Temperature readings were apparently performed properly at Bell. SCEC measured an average temperature of 1776°R. The thermocouple installed in the site flare displayed an average temperature of 2010°R. A difference of 234° is observed between the two temperature probes.

It is believed that the temperature readings from the installed thermocouples in both site flares represent the actual stack temperature. The differences between SCEC's temperature measurements and the temperature displayed by the installed thermocouples at both sites are very similar. SCEC's temperature measurements are ~200° lower than both of the thermocouples installed in each

site flare. It is believed that SCEC's temperature probe is reading ~200° less than the actual stack temperature due to a calibration error.

Engineering used the temperature readings measured by the installed thermocouples at each site in an energy balance of each system and for emission factor calculations.

LANDFILL GAS INLET FLOW RATE CORRECTIONS.

The landfill gas inlet flow meters at both sites were inaccurate. Correct landfill gas inlet flow rates were determined by performing a carbon balance using a temperature corrected exhaust flow rate and the %CO₂ outlet value approved by M&TS. Arizona's flow meter read 345 cfm during the source test. The calculated flow rate was 242 cfm (the site's flow meter reads 43% higher). Bell's flow meter read 195 cfm while the calculated flow rate was 316 cfm (the site's flow meter reads 38% lower).

Engineering used the corrected inlet flow rates in an energy balance of each systems and for emission factors calculations.

LANDFILL GAS METHANE CONCENTRATION CORRECTIONS.

Arizona Street Landfill Gas Flare Source Test Report.

Run #3 of the particulates testing was the only run that was used for energy balance and emission factors calculations. Runs #1 and #2 were eliminated from the average by M&TS.

An average inlet methane content of 390,000 ppm was approved by M&TS for Arizona. This average included an unrealistic methane content of 120,000 ppm. This approved methane concentration is incorrect as demonstrated by an energy balance of the system. See spreadsheet #1. An inlet methane content of 600,000 ppm is more accurate based on both a hydrogen and energy balance of the system. See spreadsheet #2. Past inlet sampling conducted by the site supports this value. Therefore, a methane content of 600,000 ppm was used by Engineering to calculate the emission factors for Arizona Street.

60%

Bell Junior High School Landfill Flare Source Test Report.

Run #1 of the particulates testing is believed to be the best data obtained for the energy balance and emission factor calculations. Run #2 was eliminated from the average by M&TS. Run #3 is ignored by Engineering because the percent H₂O at the outlet is too high relative to the percent CO₂ at the outlet. The percent of H₂O at the outlet should equal the percent of CO₂ at the outlet for an inlet methane content of 50%.

An average inlet methane content of 253,333 ppm was approved by M&TS for Bell. The average included an unrealistic methane content of 160,000 ppm. This approved methane concentration is incorrect as demonstrated by an energy balance on the system. See spreadsheet #3. An inlet methane content of 550,000 ppm is more accurate based on both a hydrogen and energy balance of the system. See spreadsheet #4. Therefore, a methane content of 550,000 ppm was used by Engineering to calculate the emission factors for Bell.

TOXIC AIR CONTAMINANTS.

The GC analyses of toxic air contaminants (TAC's) as approved by M&TS shows that both sites have similar compositions of TAC's. Table 2 and 3 presents the TAC's destruction efficiencies for both sites. Inlet and outlet detection limits were used when non-detectable concentrations were reported.

Table 2. Destruction Efficiency of TAC's at Arizona Street Flare.

Contaminant	Inflow Conc., lbm/hr	Outflow Conc., lbm/hr	Destruction Efficiency, %
Vinyl Chloride	0.0024	<0.00044 (ND)	>81.7
Methylene Chloride	0.0010	0.00008	91.8
Chloroform	<0.0005 (ND)	<0.00044 (ND)	>12
1,2-Dichloroethane	<0.0005 (ND)	<0.00044 (ND)	>12
1,1,1-Trichloroethane	0.0025	<0.00044 (ND)	>82.4
Benzene	0.00056	0.0003	38.2
Carbon Tetrachloride	<0.0005 (ND)	<0.00044 (ND)	>12
Trichloroethene	0.0038	<0.00044 (ND)	>88.4
1,2-Dibromoethane	<0.0005 (ND)	<0.00044 (ND)	>12
Tetrachloroethene	0.0079	<0.00044 (ND)	>94.4

Table 3. Destruction Efficiency of TAC's at Bell Jr. High Flare.

Contaminant	Inflow Conc., lbm/hr	Outflow Conc., lbm/hr	Destruction Efficiency, %
Vinyl Chloride	0.0012	<0.00028 (ND)	>76.7
Methylene Chloride	0.0029	<0.00028 (ND)	>90.5
Chloroform	<0.0004 (ND)	<0.00029 (ND)	>29.3
1,2-Dichloroethane	<0.0004 (ND)	<0.00028 (ND)	>30.0
1,1,1-Trichloroethane	0.0014	<0.00028 (ND)	>79.7
Benzene	0.0027	0.00038	85.9
Carbon Tetrachloride	<0.0004 (ND)	<0.00027 (ND)	>32.5
Trichloroethene	0.011	<0.00027 (ND)	>97.5
1,2-Dibromoethane	<0.0004 (ND)	<0.00028 (ND)	>30.0
Tetrachloroethene	0.017	<0.00027 (ND)	>98.4

LANDFILL GAS FLARE EMISSION FACTORS.

Emission factors for SO_x, NO_x, CO, and particulates were calculated using M&TS approved emissions, the corrected flow rate out the stack (using installed thermocouple readings), the corrected landfill gas flow rate at the inlet (using carbon balance), and the adjusted methane content at the inlet (using energy and hydrogen balance).

M&TS reported undetectable CO in the exhaust of both stacks but did not specify a detection limit. A detection limit of 10 ppm was assumed by Engineering and was used to calculate the CO emission factors.

The approved M&TS source test report showed that all non-methane hydrocarbons (ROG) were non-detectable (ppm range) at both the inlet and the outlet sampling locations for each site. It is recommended that an inlet concentration of 0.2 lbs ROG/mm BTU based on detection limits be used to estimate the landfill ROG generation rate. Using a conservative destruction efficiency of 70%, a 0.06 lbs ROG/mm BTU emission factor is recommended for permit processing.

SUMMARY AND DISCUSSION OF RESULTS.

The recommended emission factor of NO_x is relatively similar to the SCAQMD emission factor. SCAQMD emission factor for SO_x is one order of magnitude less than the recommended emission factor. This is probably due to differing of sulfur content in the landfill gas or differing sampling methodology. The recommended emission factors for CO and particulates indicate more efficient combustion than the SCAQMD emission factors.

SCAQMD's emission factor for ROG is too high. With SCAQMD's ROG emission factor, the outlet concentration of ROG would equal ~69 ppm. This value is higher than the measured ROG concentration in any of the sampled landfill gas inlets in San Diego. SCAQMD's emission factor for ROG is questionable. The recommended value based on non-detectable concentrations will be used by Engineering.

RECOMMENDATIONS.

It is recommended that these emission factors be used to calculate emissions for landfill gas flares and be used to determine a cut-off point for source testing landfill gas flares. With the recommended emission factors, landfill gas flare emissions can be estimated. Table 4 presents these estimated emissions.

Table 4. Estimated Emissions from Landfill Gas Flares.

Landfill Size, tons	Gas Gen. Rate, mm cu ft/yr	Estimated Emissions, tons/yr*				
		NOx	ROG	CO	Particulates	SOx
1,000,000	85.6	2.0	1.2	0.4	0.4	0.2
2,000,000	171.4	4.0	2.4	0.8	0.8	0.4
4,000,000	343	8.0	4.8	1.6	1.6	0.8
6,000,000	514	12.0	7.2	2.4	2.4	1.2
10,000,000	857	20.0	12.0	4.0	4.0	2.0

* Assumes an inlet methane content of 50%.

A landfill with a size of 9,000,000 tons and a continuous operating flare triggers Rule 20.2. A landfill with a size of 5,000,000 tons would require offsets per the proposed New Source Review. It is recommended that the presented emission factors be used to estimate emissions from landfills with a size of <5,000,000 tons. Source testing is recommended for landfills with a size of $\geq 5,000,000$ tons.

TEST SUMMARY OF LANDFILL GAS THERMAL OXIDIZER AT BALBOA PARK IN SAN DIEGO

1. Narrative Summary
2. Test Summary
3. Engineering Report
4. SOx Average
 - Run #1
 - Run #2
 - Run #3
5. NOx and CO Analysis
6. Runs #1 - #3 GC Analysis
7. Particulates
8. Test Witness
 - Run #1
 - Run #2
 - Run #3

Purpose: The SDAPCD engineering division requested testing of emissions from a landfill gas thermal oxidizer located at the Arizona Street landfill. Data regarding emissions from this type of operation were needed for regulatory decision making. The objective of these tests was to quantify emissions of speciated organic gases, oxides of nitrogen, carbon monoxide, oxides of sulfur and particulates. An additional objective was to assess the efficiency of the thermal oxidizer in destroying incoming toxic organic compounds.

Methods: Organic gases were collected in summa polished stainless steel canisters and analyzed using gas chromatography as detailed in the attached appendix. Particulate matter and oxides of sulfur were collected and determined according to modified EPA Methods 5 and 8. Oxides of nitrogen and carbon monoxide were determined using SDAPCD Method 20. A copy of the protocol and referenced methods are contained in an appendix to this report. In general, testing was accomplished in accordance with agreed upon methodology. Individual sample runs which were determined to be substantively in error were deleted from data used in the attached summary table.

Process Description: Gases are generated from the decomposition or volatilization of previously deposited waste at the landfill. A gas collection system has been installed at this site to gather these gases for processing. The collected landfill gases are oxidized in an enclosed flare. Emissions associated with this incineration are quantified in the test program discussed in this report.

Conclusions: As indicated in the attached table of summarized results, emissions of oxides of sulfur, carbon monoxide and particulate matter are quite low. Emissions of oxides of nitrogen are also fairly low as would be expected from a low heating value fuel. Emissions of hydrocarbons, including various halogenated toxic species, are also quite low.

Test Summary of Landfill Gas Thermal Oxidizer
SOURCE TEST OF VARIOUS POLLUTANTS EMITTED TO THE ATMOSPHERE

SITE: Balboa Park Landfill Gas Thermal Oxidizer
 2850 Pershing Dr.
 San Diego, CA

TEST WITNESS - SUMMARY

TEST#: 92090

P.O.#: none

TEST DATE: 3/30/92

UNIT TESTED: INCINERATOR

EQUIPMENT: LANDFILL GAS THERMAL OXIDIZER

TESTED BY: Russ Logan & Ted Jackman of SCEC

DATE: 3/30/92

SITE PERSONNEL: Ray Purtee

DATE: 3/30/92

APCD ENGINEER: Archi de la Cruz

DATE: 3/30/92

LAB ANALYSIS BY: SCEC

DATE: 4/21/92

REPORT BY: SCEC (Russ Logan)

DATE: 5/14/92

REVIEWED BY: David N. Shina

DATE: 8/5/92

APPROVED BY:

DATE: 10/1/92

JUDITH LAKE, CHIEF OF MONITORING

This report has been reviewed and found to be representative of the testing that was performed.

SO₂ TEST RESULTS SUMMARY:

ITEM	I	SO ₃			SO ₂			Total SO _x		
		Cs	Cs(12%)	E	Cs	Cs(12%)	E	Cs	Cs(12%)	E
UNITS	%	gr/dscf	gr/dscf	lbs/hr	gr/dscf	gr/dscf	lbs/hr	gr/dscf	gr/dscf	lbs/hr
VALUE	106	0.001400	0.002138	0.0388	0.000915	0.001397	0.0254	0.002315	0.003535	0.0642

CO TEST RESULTS SUMMARY:

GAS	TEST (PPM)	LIMITS (PPM)	PERFORMANCE EXCEEDANCE/NON-EXCEEDANCE
NO _x	29.49	N/A	N/A
CO	0.00	N/A	N/A

PARTICULATE TEST RESULTS SUMMARY

ITEM	ts	Bws	%O ₂	%CO ₂	vs	Qstd	Cs(total)	Cs(12% total)	E(total)	%I
UNITS	°F	%	%	%	ft/sec	dscfm	gr/hr	gr/hr	lbs/hr	%
VALUE	1437	8.67	11.70	7.81	17.419	3246	0.0316	0.0050	0.09	108

G.C. TEST RESULTS SUMMARY:

	AVERAGE INLET		AVERAGE OUTLET			AVERAGE INLET		AVERAGE OUTLET	
	RESULT (PPM)	DET. LIMIT (PPM)	RESULT (PPM)	DET. LIMIT (PPM)		RESULT (PPB)	DET. LIMIT (PPB)	RESULT (PPB)	DET. LIMIT (PPB)
C1 as Methane	390000	118	25	3.7	Vinyl Chloride	970	186	ND	14.6
C2 as Ethane	ND	118	ND	2.7	Methylene Chloride	303	133	2	10.8
C3 as n-Propane	ND	93	ND	2.9	Chloroform	ND	97	ND	7.6
C4 as n-Butane	ND	72	ND	2.3	1,2-Dichloroethane	ND	115	ND	8.1
C5 as Pentane	ND	47	ND	1.5	1,1,1-Trichloroethane	464	86	ND	6.8
C6 as n-Hexane	ND	47	ND	1.5	Benzene	180	147	8	11.6
C7 as n-Heptane	ND	47	ND	1.5	Carbon Tetrachloride	ND	74	ND	5.9
C8 as n-Octane	ND	47	ND	1.5	Trichloroethane	723	86	ND	6.9
C9 as n-Nonane	ND	47	ND	1.5	1,2-Dibromoethane	ND	61	ND	4.8
C10 as n-Decane	ND	47	ND	1.5	Tetrachloroethane	1213	68	ND	5.5

ENGINEERING SOURCE TEST REPORT ARIZONA STREET LANDFILL GAS FLARE

DATE: April 10, 1992
SOURCE: Arizona Street Landfill
EQUIPMENT: Arizona Street Landfill Gas Flare
ENGINEER: Archi dela Cruz 

TEST PURPOSE

The purpose of this source test is to more accurately assess PM, CO, NO_x, SO₂, and TOG/ROG emissions which are generated at this type of source. Also, there will be an analysis of toxic emissions generated at the inlet and outlet of the landfill gas flare system. The results of this source test will be used to generate emission factors for this type of source.

BACKGROUND INFORMATION

SDAPCD M&TS personnel: Dave Shina and Janet Cawyer
Contracted source testing company: Russ Logan
Operator of flare: South Coast Environmental Company
Ray Purtee, City of San Diego

OPERATING PARAMETERS DURING TESTING

The flare was in operation upon arrival. Scaffolding and newly positioned sampling ports were provided. The following parameters were observed during the source test.

Sampling date:	March 30, 1992
Starting time of sampling:	11:25 am
Ending time of sampling:	5:15 pm
Average landfill gas flowrate:	345 cfm
Natural gas usage:	0 cfm
Average flare temperature:	1650 F
Average landfill O ₂ content:	0.022%
Methane content of landfill gas	48% (as reported by Ray Purtee)

DISCUSSION AND CONCLUSION.

One event that occurred during the source test was that the flowmeter was recalibrated. While I was recording the O₂ content and observing the stack, I noticed Ray Purtee and Greg Montgomery (Klienfelder) in front of the flowmeter. I approached them. They indicated that they were clearing the vent valves from condensation. It appeared that clearing the vent valves would have little effect on the operating system (vent pipes are approximately 1/8" in diameter). The vent valves were opened for about only a minute each. The flowrate through the vent valves was assumed to be negligible.

Later, I noticed that the flowrate readings decreased from 360 cfm to 160 cfm. I called Ray Purtee (he had left the site), and asked him about this occurrence. Ray Purtee returned to the site and realized that Greg Montgomery had recalibrated the flowmeter. Purtee explained that Montgomery reset the flowmeter to zero while clearing the vent valves.

I question the validity of the flowmeter readings which I recorded. Two average landfill gas flowrates were calculated. The first average flowrate calculated (345 cfm) represents the average flowrate prior to the flowmeter recalibration by Montgomery. A second average flowrate was calculated (250 cfm) represents the average flowrate after the flowmeter recalibration. I believe that the more representative average flowrate value would be 345 cfm.

The landfill gas flare system appeared to be operating under typical conditions during testing. No noticeable operating changes were observed throughout the testing. The system appeared to be in good operating condition. No visible emissions were observed during the testing. Slight landfill gas odors were observed in the vicinity of the blower but at non-detectable levels from the explosimeter (ID#168241, calibrated for propane).

The source was not operating under S/A conditions. The source was not controlling off-site migration from the landfill. This implies there is an abundance of landfill gas and does not effect the source test results.

Landfill Flare Source Test Data Arizona Street Landfill

Warm-up time to reach operating temperature - none required

~~TIME~~ no visible emission, ~~11.025%~~

TEMP. = 1652°F, O₂ % ~~11.025%~~, 340 ~~ft³/min~~ cfm

SLEC arrived at 8:30 slight odor but no reading on explosimeter

1st run of PM? low pressure differential in stack = ~0.05" H₂O

SOURCE TESTING RUN #1

TIME, min	LANDFILL GAS BURNED, ft ³ /min (inlet)	NATURAL GAS USAGE, ft ³ /min	TEMP, °F	O ₂ CONTENT
1:25 PM	340 340	0	1653	0.025%
5	320 320		1650	0.023%
10	360 360		1655	0.023%
15	340 340		1652	0.023%
20	340 340		1650	0.022%
25	340 340		1650	0.022%
30	340 340		1649	0.022%
35	320 320		1648	0.022%
40	340 340		1651	0.022%
45	360 360		1649	0.022%
50	360 360		1653	0.022%
55	360 360		1653	0.022%
10	360 360		1647	0.022%
20	340		1654	0.022%
30	360		1649	"
40	300		1650	"
50	160		1650	"
10	200		1657	"

90 car out
of ice

90

10

Landfill Flare Source Test Data Arizona

TIME	MIN. PASSED	LANDFILL GAS INLET, cfm	NAT'L GAS INLET, cfm	TEMP., °F	O ₂ CONTE
1:30 phone	95	200	0	1651	0.022%
2:00	135	280	0	1650	0.02
2:20		280	0	1652	0.022

Ray Purtee cleaned valves of flowmeter. ~~Stated~~ Purtee stated clearing valves will have few drops of condensate came out. little effects of system.

Ray Purtee stated Greg Montgomery (Kleintfelder) "recalibrated" flowmeter in the middle of source testing. Montgomery turned bottom screw to zero the flowmeter w/ his thumbnail. Purtee has scaffolding until Apr. 13.

2:55		260	0	1652	0.022%
3:15		280	1647	1647	0.022%
3:00		280	0	1655	0.022%
3:40		260	↓	1651	0.022%
3:20		260		1652	0.022%
3:30		260		1650	"
3:40		260		1652	"
3:50		260		1653	"
4:00		260		1648	"

SOURCE TEST OF OXIDES OF SULFUR EMISSIONS TO THE ATMOSPHERE

Test Witness - Average (SOx)

TEST RESULTS SUMMARY:

ITEM	I	SO3			SO2			Total SOx		
		Cs	Cs(12%)	E	Cs	Cs(12%)	E	Cs	Cs(12%)	E
UNITS	%	gr/dscf	gr/dscf	lbs/hr	gr/dscf	gr/dscf	lbs/hr	gr/dscf	gr/dscf	lbs/hr
VALUE	106	0.001400	0.002138	0.0388	0.000915	0.001397	0.0254	0.002315	0.003535	0.0642

TEST PARAMETERS:

PROCEDURES:

The procedures and equipment utilized in these tests are based on EPA NSPS guidelines and from the EPA CFR 40, Standards Method 8. The sampling utilized a front-end filter (fig. 1).

CALCULATIONS:

All calculations are based on the EPA CFR 40, July 1, 1991, Parts 53-60, Appendix A, Method 8.

SAMPLING:

The test consisted of sampling at 16 traverse points, 4 from each of 4 sample ports (fig.2), collected from 84 inches below the stack (fig.3). All field data were transferred to the computer printout. All calculations were done by the computer.

ANALYSES:

Gas: A CEM analysis was performed by SCEC.

SOx: All procedures follow EPA guidelines, except where noted in this report.

EQUIPMENT:

All testing and analysis equipment was calibrated according to EPA guidelines and performed by SCEC.

OVERVIEW OF THE TEST:

	RUN #1	RUN #2	RUN #3
SAMPLING:	Failed	Passed	Passed
LABORATORY:	Passed	Passed	Passed

#1 was eliminated from the overall test average because QA criteria were not met. (See the laboratory sheet of the particulate report for an in depth explanation.)

$$\text{Concentration(H}_2\text{SO}_4) = [\text{K} \cdot \text{Normality} \cdot \text{V-titrant} \cdot (\text{V-solution/V-aliquot})] / \text{Vm}-(\text{std})$$

$$\text{Concentration(SO}_2) = [\text{K} \cdot \text{Normality} \cdot \text{V-titrant} \cdot (\text{V-solution/V-aliquot})] / \text{Vm}-(\text{std})$$

$$\text{K} = \text{MW} / \# \text{equiv/mole}$$

CALCULATIONS:

TOTAL SO3

Conc(H2SO4,total) = $\sum \text{Conc(H}_2\text{SO}_4, \text{location})$	0.0000674	0.0000826	0.0000989	0.0000908	grams/dscf
Cs(H2SO4,total) = $\sum \text{Cs(H}_2\text{SO}_4, \text{location})$	0.0010403	0.0012752	0.0015257	0.0014085	grains/dscf
Cs(H2SO4,12%,total) = $\sum \text{Cs(H}_2\text{SO}_4, 12\%, \text{location})$	0.0015546	0.0019321	0.0023442	0.0021382	grains/dscf
E (H2SO4,total) = $\sum \text{E(H}_2\text{SO}_4, \text{location})$	0.0245	0.0352	0.0424	0.0388	lbs/hr

TOTAL SO2

Conc(SO2,total) = $\sum \text{Conc(SO}_2, \text{location})$	0.0000440	0.0000540	0.0000646	0.0000593	grams/dscf
Cs(SO2,total) = $\sum \text{Cs(SO}_2, \text{location})$	0.0006795	0.0008329	0.0009965	0.0009147	grains/dscf
Cs(SO2,12%,total) = $\sum \text{Cs(SO}_2, 12\%, \text{location})$	0.0010154	0.0012620	0.0015311	0.0013965	grains/dscf
E (SO2,total) = $\sum \text{E(SO}_2, \text{location})$	0.0160	0.0230	0.0277	0.0254	lbs/hr

TOTAL SOx

Conc(SOx,total) = Conc(H2SO4,total) + Conc(SO2,total)	0.0001115	0.0001366	0.0001635	0.0001500	grams/dscf
Cs(SOx,total) = Cs(H2SO4,total) + Cs(SO2,total)	0.0017198	0.0021081	0.0025222	0.0023151	grains/dscf
SO2,12%,total) = Cs(H2SO4,12%,total) + Cs(SO2,12%,total)	0.0025700	0.0031941	0.0038753	0.0035347	grains/dscf
E(SOx,total) = E(H2SO4,total) + E(SO2,total)	0.0405	0.0582	0.0702	0.0642	lbs/hr

** Run #1 is eliminated from the overall test average

SOURCE TEST OF OXIDES OF SULFUR EMISSIONS TO THE ATMOSPHERE

Test Witness - Average (SOx)

TEST RESULTS SUMMARY:

ITEM	I	SO3			SO2			Total SOx		
		Cs	Cs(12%)	E	Cs	Cs(12%)	E	Cs	Cs(12%)	E
UNITS	%	gr/dscf	gr/dscf	lbs/hr	gr/dscf	gr/dscf	lbs/hr	gr/dscf	gr/dscf	lbs/hr
VALUE	106	0.001400	0.002138	0.0388	0.000915	0.001397	0.0254	0.002315	0.003535	0.0642

TEST PARAMETERS:

PROCEDURES:

The procedures and equipment utilized in these tests are based on EPA NSPS guidelines and from the EPA CFR 40, Standards Method 8. The sampling utilized a front-end filter (fig. 1).

CALCULATIONS:

All calculations are based on the EPA CFR 40, July 1, 1991, Parts 53-60, Appendix A, Method 8.

SAMPLING:

The test consisted of sampling at 16 traverse points, 4 from each of 4 sample ports (fig.2), collected from 84 inches below the stack (fig.3). All field data were transferred to the computer printout. All calculations were done by the computer.

ANALYSES:

Gas: A CEM analysis was performed by SCEC.

SOx: All procedures follow EPA guidelines, except where noted in this report.

EQUIPMENT:

All testing and analysis equipment was calibrated according to EPA guidelines and performed by SCEC.

OVERVIEW OF THE TEST:

	RUN #1	RUN #2	RUN #3
SAMPLING:	Failed	Passed	Passed
LABORATORY:	Passed	Passed	Passed

#1 was eliminated from the overall test average because QA criteria were not met. (See the laboratory sheet of the particulate report for depth explanation.)

$$\text{Concentration(H}_2\text{SO}_4) = [\text{K} \cdot \text{Normality} \cdot \text{V-titrant} \cdot (\text{V-solution}/\text{V-aliquot})] / \text{Vm}-(\text{std})$$

$$\text{Concentration(SO}_2) = [\text{K} \cdot \text{Normality} \cdot \text{V-titrant} \cdot (\text{V-solution}/\text{V-aliquot})] / \text{Vm}-(\text{std})$$

$$\text{K} = \text{MW}/\# \text{equiv/mole}$$

CALCULATIONS:

TOTAL SO3

Conc(H2SO4,total) = ΣConc(H2SO4,location) =	0.0000674	0.0000826	0.0000989	0.0000908	grams/dscf
Cs(H2SO4,total) = ΣCs(H2SO4,location) =	0.0010403	0.0012752	0.0015257	0.0014085	grains/dscf
Cs(H2SO4,12%,total) = ΣCs(H2SO4,12%,location) =	0.0015546	0.0019321	0.0023442	0.0021382	grains/dscf
E (H2SO4,total) = ΣE(H2SO4,location) =	0.0245	0.0352	0.0424	0.0388	lbs/hr

TOTAL SO2

Conc(SO2,total) = ΣConc(SO2,location) =	0.0000440	0.0000540	0.0000646	0.0000593	grams/dscf
Cs(SO2,total) = ΣCs(SO2,location) =	0.0006795	0.0008329	0.0009965	0.0009147	grains/dscf
Cs(SO2,12%,total) = ΣCs(SO2,12%,location) =	0.0010154	0.0012620	0.0015311	0.0013965	grains/dscf
E (SO2,total) = ΣE(SO2,location) =	0.0160	0.0230	0.0277	0.0254	lbs/hr

TOTAL SOx

Conc(SOx,total) = Conc(H2SO4,total)+Conc(SO2,total) =	0.0001115	0.0001366	0.0001635	0.0001500	grams/dscf
Cs(SOx,total) = Cs(H2SO4,total)+Cs(SO2,total) =	0.0017198	0.0021081	0.0025222	0.0023151	grains/dscf
SO2,12%,total) = Cs(H2SO4,12%,total)+Cs(SO2,12%,total) =	0.0025700	0.0031941	0.0038753	0.0035347	grains/dscf
E(SOx,total) = E(H2SO4,total)+E(SO2,total) =	0.0405	0.0582	0.0702	0.0642	lbs/hr

** Run #1 is eliminated from the overall test average

Test Witness - Run #1 (SOx)**TEST RESULTS SUMMARY:**

ITEM	I	SO3			SO2			Total SOx		
		Cs	Cs(12%)	E	Cs	Cs(12%)	E	Cs	Cs(12%)	E
UNITS	%	gr/dscf	gr/dscf	lbs/hr	gr/dscf	gr/dscf	lbs/hr	gr/dscf	gr/dscf	lbs/hr
VALUE	106	0.001040	0.001555	0.0245	0.000679	0.001015	0.0160	0.001720	0.002570	0.0485

TEST PARAMETERS:**OVERVIEW OF THE TEST****SAMPLING:** Failed**LABORATORY:** Passed

The data from this test is unacceptable and will not be used in the overall test average (see the particulate laboratory report-Run #1 for an in depth explanation).

$$\text{Concentration}(\text{H}_2\text{SO}_4) = [\text{K} * \text{Normality} * \text{V-titrant} * (\text{V-solution} / \text{V-aliquot})] / \text{Vm}(\text{std})$$

CALCULATIONS:

SCCELLANEEOUS DATA

N = Normality =

Vmstd =

Qstd =

%CO₂ =

15.43 grains = 1 gram

7000grains=1lb, 60min=1hr; 60min/hr/7000grains/lb=

SO₃ as H₂SO₄:

MW =

equiv/mole vs. BaCl₂ =

K =

FRONT HALF

Volume of the titrant = Vt

Volume of the solution = Vsoln =

Volume of the aliquot = Valiquot =

Conc(H₂SO₄,front) = $[\text{K} * \text{N} * \text{Vt} * (\text{Vsoln} / \text{Valiquot})] / \text{Vm}(\text{std}) =$

Cs(H₂SO₄,front) = 15.43 * Conc(H₂SO₄,front) =

Cs(H₂SO₄,12%,front) = Cs(front) * (12/%CO₂) =

E (H₂SO₄,front) = 0.00857 * Qstd * Cs(H₂SO₄,front) =

FILTER

Volume of the titrant = Vt

Volume of the solution = Vsoln =

Volume of the aliquot = Valiquot =

Conc(H₂SO₄,filter) = $[\text{K} * \text{N} * \text{Vt} * (\text{Vsoln} / \text{Valiquot})] / \text{Vm}(\text{std}) =$

Cs(H₂SO₄,filter) = 15.43 * Conc(H₂SO₄,filter) =

Cs(H₂SO₄,12%,filter) = Cs(filter) * (12/%CO₂) =

E (H₂SO₄,filter) = 0.00857 * Qstd * Cs(H₂SO₄,filter) =

BACK HALF

Volume of the titrant = Vt

Volume of the solution = Vsoln =

Volume of the aliquot = Valiquot =

Conc(H₂SO₄,back) = $[\text{K} * \text{N} * \text{Vt} * (\text{Vsoln} / \text{Valiquot})] / \text{Vm}(\text{std}) =$

Cs(H₂SO₄,back) = 15.43 * Conc(H₂SO₄,back) =

Cs(H₂SO₄,12%,back) = Cs(H₂SO₄,back) * (12/%CO₂) =

E (H₂SO₄,back) = 0.00857 * Qstd * Cs(H₂SO₄,back) =

TOTAL SO₃

Conc(H₂SO₄,total) = $\sum \text{Conc}(\text{H}_2\text{SO}_4, \text{location})$

Cs(H₂SO₄,total) = $\sum \text{Cs}(\text{H}_2\text{SO}_4, \text{location}) =$

Cs(H₂SO₄,12%,total) = $\sum \text{Cs}(\text{H}_2\text{SO}_4, 12\%, \text{location}) =$

E (H₂SO₄,total) = $\sum \text{E}(\text{H}_2\text{SO}_4, \text{location}) =$

SDAPCD	SCEC
0.00971	0.00971 equiv/liter
30.794	30.79 dscf
2749	2727 dscfm
8.03	8.03 %
15.43	15.4 grains/gram
0.00857	0.00857 lbs-min/grs-hr

98.08	** 97 g/mole
2	2 equiv/mole
49.04	48.5 grams/equiv

0	0 ml
545	545 ml
10	10 ml
0.0000000	0.0000000 grams/dscf
0.0000000	0.0000000 grains/dscf
0.0000000	0.0000000 grains/dscf
0.0000	0.0000 lbs/hr

0	0 ml
100	100 ml
10	10 ml
0.0000000	0.0000000 grams/dscf
0.0000000	0.0000000 grains/dscf
0.0000000	0.0000000 grains/dscf
0.0000	0.0000 lbs/hr

0.08	0.08 ml
545	545 ml
10	10 ml
0.0000674	0.0000667 grams/dscf
0.0010403	0.0010270 grains/dscf
0.0015546	0.0015347 grains/dscf
0.0245	0.0242 lbs/hr

0.0000667	grams/dscf
0.0010270	grains/dscf
0.0015347	grains/dscf
0.0242	lbs/hr

COMMENTS:

** SCEC used an incorrect molecular weight for H₂SO₄, and this gave incorrect values for all the subsequent numbers that SCEC generated in its final report.

The District will use the numbers generated by the District's spreadsheet, because these values are correct.

$$\text{Concentration}(\text{SO}_2) = [\text{K} * \text{Normality} * \text{V-titrant} * (\text{V-solution} / \text{V-aliquot})] / \text{Vm}-(\text{std})$$

CALCULATIONS:

SCCELLANEOUS DATA

N = Normality =

Vmstd =

Qstd =

%CO2 =

15.43 grains = 1 gram

7000grains=1lb, 60min=1hr; 60min/hr/7000grains/lb=

SO2:

MW =

equiv/mole vs. BaCl2 =

K =

FRONT HALF

Volume of the titrant = Vt

Volume of the solution = Vsoln =

Volume of the aliquot = Valiquot =

Conc(SO2,front) = $[\text{K} * \text{N} * \text{Vt} * (\text{Vsoln} / \text{Valiquot})] / \text{Vm}(\text{std}) =$

Cs(SO2,front) = 15.43 * Conc(SO2,front) =

Cs(SO2,12%,front) = Cs(SO2,front) * (12/%CO2) =

E (SO2,front) = 0.00857 * Qstd * Cs(SO2,front) =

FILTER

Volume of the titrant = Vt

Volume of the solution = Vsoln =

Volume of the aliquot = Valiquot =

Conc(SO2,filter) = $[\text{K} * \text{N} * \text{Vt} * (\text{Vsoln} / \text{Valiquot})] / \text{Vm}(\text{std}) =$

Cs(SO2,filter) = 15.43 * Conc(SO2,filter) =

Cs(SO2,12%,filter) = Cs(SO2,filter) * (12/%CO2) =

E (SO2,filter) = 0.00857 * Qstd * Cs(SO2,filter) =

BACK HALF

Volume of the titrant = Vt

Volume of the solution = Vsoln =

Volume of the aliquot = Valiquot =

Conc(SO2,back) = $[\text{K} * \text{N} * \text{Vt} * (\text{Vsoln} / \text{Valiquot})] / \text{Vm}(\text{std}) =$

Cs(SO2,back) = 15.43 * Conc(SO2,back) =

Cs(SO2,12%,back) = Cs(SO2,back) * (12/%CO2) =

E (SO2,back) = 0.00857 * Qstd * Cs(SO2,back) =

TOTAL SO2

Conc(SO2,total) = $\sum \text{Conc}(\text{SO}_2, \text{location})$

Cs(SO2,total) = $\sum \text{Cs}(\text{SO}_2, \text{location}) =$

Cs(SO2,12%,total) = $\sum \text{Cs}(\text{SO}_2, 12\%, \text{location}) =$

E (SO2,total) = $\sum \text{E}(\text{SO}_2, \text{location}) =$

SDAPCD	SCEC
0.00971	0.00971 equiv/liter
30.794	30.79 dscf
2749	2727 dscfm
8.03	8.03 %
15.43	15.4 grains/gram
0.00857	0.00857 lbs-min/grs-hr

64.06

not done g/mole

2

not done equiv/mole

32.03

not done grams/equiv

0	not done ml
545	not done ml
10	not done ml
0.0000000	not done grams/dscf
0.0000000	not done grains/dscf
0.0000000	not done grains/dscf
0.0000	not done lbs/hr

0	not done ml
100	not done ml
10	not done ml
0.0000000	not done grams/dscf
0.0000000	not done grains/dscf
0.0000000	not done grains/dscf
0.0000	not done lbs/hr

0.08	not done ml
545	not done ml
10	not done ml
0.0000440	not done grams/dscf
0.0006795	not done grains/dscf
0.0010154	not done grains/dscf
0.0160	not done lbs/hr

not done grams/dscf
not done grains/dscf
not done grains/dscf
not done lbs/hr

COMMENTS:

SCEC did not calculate the contribution due to SO2; so, the District will use the values generated by the District's spreadsheet.

COMPANY: ARIZONA STREET
 DATE: 3/30/92
 UNIT: FLARE
 REPORT #: T1482-1

RUN #1
 @ 68°F
 EPA METHOD 5/8

PARTICULATE RESULTS:	net mg	gr/dscf	gr/scf	gr/dscf @ 12% CO2	lbs/hr
Probe & Nozzle:	0	0	0	0	0
Filter:	0	0	0	0	0
Condensables:	16.895	0.008450	0.007713	0.012628	0.2
Total:	16.895	0.008450	0.007713	0.012628	0.2

N BaCl = 0.00971

SULFATE RESULTS:	Vol aliq	Vt	gr/dscf	gr/scf	gr/dscf @ 12% CO2	lbs/hr
Probe & Nozzle:	54.5	0	0	0	0	0
Filter:	10	0	0	0	0	0
Condensables:	54.5	0.08	0.001026	0.000937	0.001534	0.02
Total:			0.001026	0.000937	0.001534	0.02

ADDITIONAL DATA:

TIME		%O2	%CO2	%H2O	Vm(std)	SDCFM
start	finish					
1125	1309	11.55	8.03	8.72	30.79	2727

*only run # 3 were used for cal. of
 emissions*

Test Witness - Run #2 (SOx)

TEST RESULTS SUMMARY:

ITEM	I	SO3			SO2			Total SOx		
		Cs	Cs(12%)	E	Cs	Cs(12%)	E	Cs	Cs(12%)	E
UNITS	%	gr/dscf	gr/dscf	lbs/hr	gr/dscf	gr/dscf	lbs/hr	gr/dscf	gr/dscf	lbs/hr
VALUE	103	0.001275	0.001932	0.0352	0.000833	0.001262	0.0230	0.002108	0.003194	0.0582

TEST PARAMETERS:

OVERVIEW OF THE TEST

SAMPLING: Passed

LABORATORY: Passed

The data from this test is acceptable and will be used in the overall test average.

$$\text{Concentration}(\text{H}_2\text{SO}_4) = [\text{K} * \text{Normality} * \text{V-titrant} * (\text{V-solution} / \text{V-aliquot})] / \text{Vm}-(\text{std})$$

CALCULATIONS:

SCCELLANEUS DATA

N = Normality =

Vmstd =

Qstd =

%CO2 =

15.43 grains = 1 gram

7000grains=1lb, 60min=1hr; 60min/hr/7000grains/lb=

SO3 as H2SO4:

MW =

equiv/mole vs. BaCl2 =

K =

FRONT HALF

Volume of the titrant = Vt

Volume of the solution = Vsoln =

Volume of the aliquot = Valiquot =

Conc(H2SO4,front) = $[\text{K} * \text{N} * \text{Vt} * (\text{Vsoln} / \text{Valiquot})] / \text{Vm}(\text{std}) =$

Cs(H2SO4,front) = 15.43 * Conc(H2SO4,front) =

Cs(H2SO4,12%,front) = Cs(front) * (12/%CO2) =

E (H2SO4,front) = 0.00857 * Qstd * Cs(H2SO4,front) =

FILTER

Volume of the titrant = Vt

Volume of the solution = Vsoln =

Volume of the aliquot = Valiquot =

Conc(H2SO4,filter) = $[\text{K} * \text{N} * \text{Vt} * (\text{Vsoln} / \text{Valiquot})] / \text{Vm}(\text{std}) =$

Cs(H2SO4,filter) = 15.43 * Conc(H2SO4,filter) =

Cs(H2SO4,12%,filter) = Cs(filter) * (12/%CO2) =

E (H2SO4,filter) = 0.00857 * Qstd * Cs(H2SO4,filter) =

BACK HALF

Volume of the titrant = Vt

Volume of the solution = Vsoln =

Volume of the aliquot = Valiquot =

Conc(H2SO4,back) = $[\text{K} * \text{N} * \text{Vt} * (\text{Vsoln} / \text{Valiquot})] / \text{Vm}(\text{std}) =$

Cs(H2SO4,back) = 15.43 * Conc(H2SO4,back) =

Cs(H2SO4,12%,back) = Cs(H2SO4,back) * (12/%CO2) =

E (H2SO4,back) = 0.00857 * Qstd * Cs(H2SO4,back) =

TOTAL SO3

Conc(H2SO4,total) = $\sum \text{Conc}(\text{H}_2\text{SO}_4, \text{location})$

Cs(H2SO4,total) = $\sum \text{Cs}(\text{H}_2\text{SO}_4, \text{location}) =$

Cs(H2SO4,12%,total) = $\sum \text{Cs}(\text{H}_2\text{SO}_4, 12\%, \text{location}) =$

E (H2SO4,total) = $\sum \text{E}(\text{H}_2\text{SO}_4, \text{location}) =$

SDAPCD	SCEC
0.00971	0.00971 equiv/liter
35.262	35.25 dscf
3223	3402 dscfm
7.92	7.92 %
15.43	15.4 grains/gram
0.00857	0.00857 lbs-min/grs-hr

98.08	** 97 g/mole
2	2 equiv/mole
49.04	48.5 grams/equiv

0	0 ml
70	70 ml
10	10 ml
0.0000000	0.0000000 grams/dscf
0.0000000	0.0000000 grains/dscf
0.0000000	0.0000000 grains/dscf
0.0000	0.0000 lbs/hr

0	0 ml
100	100 ml
10	10 ml
0.0000000	0.0000000 grams/dscf
0.0000000	0.0000000 grains/dscf
0.0000000	0.0000000 grains/dscf
0.0000	0.0000 lbs/hr

0.18	0.18 ml
340	340 ml
10	10 ml
0.0000826	0.0000818 grams/dscf
0.0012752	0.0012591 grains/dscf
0.0019321	0.0019078 grains/dscf
0.0352	0.0348 lbs/hr

Conc(H2SO4,total) = $\sum \text{Conc}(\text{H}_2\text{SO}_4, \text{location})$	0.0000826	0.0000818 grams/dscf
Cs(H2SO4,total) = $\sum \text{Cs}(\text{H}_2\text{SO}_4, \text{location}) =$	0.0012752	0.0012591 grains/dscf
Cs(H2SO4,12%,total) = $\sum \text{Cs}(\text{H}_2\text{SO}_4, 12\%, \text{location}) =$	0.0019321	0.0019078 grains/dscf
E (H2SO4,total) = $\sum \text{E}(\text{H}_2\text{SO}_4, \text{location}) =$	0.0352	0.0348 lbs/hr

COMMENTS:

** SCEC used an incorrect molecular weight for H2SO4, and this gave incorrect values for all the subsequent numbers that SCEC generated in its final report.

The District will use the numbers generated by the District's spreadsheet, because these values are correct.

$$\text{Concentration(SO}_2\text{)} = [\text{K} \cdot \text{Normality} \cdot \text{V-titrant} \cdot (\text{V-solution}/\text{V-aliquot})] / \text{Vm}-(\text{std})$$

CALCULATIONS:

SCCELLANEEOUS DATA

N = Normality =

Vmstd =

Qstd =

%CO₂ =

15.43 grains = 1 gram

7000grains=1lb, 60min=1hr; 60min/hr/7000grains/lb=

SO₂:

MW =

equiv/mole vs. BaCl₂ =

K =

FRONT HALF

Volume of the titrant = V_t

Volume of the solution = V_{soln} =

Volume of the aliquot = V_{aliquot} =

Conc(SO₂,front) = $[K \cdot N \cdot V_t \cdot (V_{soln}/V_{aliquot})] / V_m(\text{std}) =$

Cs(SO₂,front) = 15.43 * Conc(SO₂,front) =

Cs(SO₂,12%,front) = Cs(SO₂,front) * (12/%CO₂) =

E (SO₂,front) = 0.00857 * Qstd * Cs(SO₂,front) =

FILTER

Volume of the titrant = V_t

Volume of the solution = V_{soln} =

Volume of the aliquot = V_{aliquot} =

Conc(SO₂,filter) = $[K \cdot N \cdot V_t \cdot (V_{soln}/V_{aliquot})] / V_m(\text{std}) =$

Cs(SO₂,filter) = 15.43 * Conc(SO₂,filter) =

Cs(SO₂,12%,filter) = Cs(SO₂,filter) * (12/%CO₂) =

E (SO₂,filter) = 0.00857 * Qstd * Cs(SO₂,filter) =

BACK HALF

Volume of the titrant = V_t

Volume of the solution = V_{soln} =

Volume of the aliquot = V_{aliquot} =

Conc(SO₂,back) = $[K \cdot N \cdot V_t \cdot (V_{soln}/V_{aliquot})] / V_m(\text{std}) =$

Cs(SO₂,back) = 15.43 * Conc(SO₂,back) =

Cs(SO₂,12%,back) = Cs(SO₂,back) * (12/%CO₂) =

E (SO₂,back) = 0.00857 * Qstd * Cs(SO₂,back) =

TOTAL SO₂

Conc(SO₂,total) = $\sum \text{Conc(SO}_2\text{,location)}$

Cs(SO₂,total) = $\sum \text{Cs(SO}_2\text{,location)}$ =

Cs(SO₂,12%,total) = $\sum \text{Cs(SO}_2\text{,12%,location)}$ =

E (SO₂,total) = $\sum \text{E(SO}_2\text{,location)}$ =

SDAPCD

SCEC

0.00971	0.00971	equiv/liter
35.262	35.25	dscf
3223	3402	dscfm
7.92	7.92	%
15.43	15.4	grains/gram
0.00857	0.00857	lbs-min/grs-hr

64.06

not done g/mole

2

not done equiv/mole

32.03

not done grams/equiv

0	not done	ml
70	not done	ml
10	not done	ml
0.0000000	not done	grams/dscf
0.0000000	not done	grains/dscf
0.0000000	not done	grains/dscf
0.0000	not done	lbs/hr

0	not done	ml
100	not done	ml
10	not done	ml
0.0000000	not done	grams/dscf
0.0000000	not done	grains/dscf
0.0000000	not done	grains/dscf
0.0000	not done	lbs/hr

0.18	not done	ml
340	not done	ml
10	not done	ml
0.0000540	not done	grams/dscf
0.0008329	not done	grains/dscf
0.0012620	not done	grains/dscf
0.0230	not done	lbs/hr

0.0000540	not done	grams/dscf
0.0008329	not done	grains/dscf
0.0012620	not done	grains/dscf
0.0230	not done	lbs/hr

COMMENTS:

SCEC did not calculate the contribution due to SO₂; so, the District will use the values generated by the District's spreadsheet.

COMPANY: ARIZONA STREET
 DATE: 3/30/92
 UNIT: FLARE
 REPORT #: T1482-1

RUN #2
 @ 68°F
 EPA METHOD 5/8

PARTICULATE RESULTS:	net mg	gr/dscf	gr/scf	gr/dscf @ 12% CO2	lbs/hr
Probe & Nozzle:	4.9	0.002140	0.001932	0.003243	0.06
Filter:	0.7	0.000305	0.000276	0.000463	0.01
Condensables:	8.33	0.003639	0.003284	0.005513	0.11
Total:	13.93	0.006085	0.005492	0.009220	0.18

N BaCl = 0.00971

SULFATE RESULTS:	Vol aliq	Vt	gr/dscf	gr/scf	gr/dscf @ 12% CO2	lbs/hr
Probe & Nozzle:	7	0	0	0	0	0
Filter:	10	0	0	0	0	0
Condensables:	34	0.18	0.001259	0.001136	0.001907	0.04
Total:			0.001259	0.001136	0.001907	0.04

ADDITIONAL DATA:

TIME		%O2	%CO2	%H2O	Vm(std)	SDCFM
start	finish					
1403	1508	11.69	7.92	9.74	35.25	3402

Test Witness - Run #3 (SOx)

TEST RESULTS SUMMARY:

ITEM	I	SO3			SO2			Total SOx		
		Cs	Cs(12%)	E	Cs	Cs(12%)	E	Cs	Cs(12%)	E
UNITS	%	gr/dscf	gr/dscf	lbs/hr	gr/dscf	gr/dscf	lbs/hr	gr/dscf	gr/dscf	lbs/hr
VALUE	108	0.001526	0.002344	0.0424	0.000996	0.001531	0.0277	0.002522	0.003875	0.0702

TEST PARAMETERS:

PROCEDURES:

The procedures and equipment utilized in these tests are based on EPA NSPS guidelines and from the EPA CFR 40, Standards Method 8. The sampling utilized a front-end filter (fig. 1).

CALCULATIONS:

All calculations are based on the EPA CFR 40, July 1, 1991, Parts 53-60, Appendix A, Method 8.

SAMPLING:

The test consisted of sampling at 16 traverse points, 4 from each of 4 sample ports (fig.2), collected from 84 inches below the stack (fig.3). All field data was transferred to the computer printout. All calculations were done by the computer.

ANALYSES:

Gas: A CEM analysis was performed by SCEC.

SOx: All procedures follow EPA guidelines, except where noted in this report.

EQUIPMENT:

All testing and analysis equipment was calibrated according to EPA guidelines and performed by SCEC.

OVERVIEW OF THE TEST

SAMPLING: Passed

LABORATORY: Passed

The data from this test is acceptable and will be used in the overall test average.

Run # 3

$$\text{Concentration}(\text{H}_2\text{SO}_4) = [\text{K} * \text{Normality} * \text{V-titrant} * (\text{V-solution} / \text{V-aliquot})] / \text{Vm}-(\text{std})$$

CALCULATIONS:

...SCCELLANEEOUS DATA

N = Normality =

Vmstd =

Qstd =

%CO2 =

15.43 grains = 1 gram

7000grains=1lb, 60min=1hr; 60min/hr/7000grains/lb=

SO3 as H2SO4:

MW =

equiv/mole vs. BaCl2 =

K =

FRONT HALF

Volume of the titrant = Vt

Volume of the solution = Vsoln =

Volume of the aliquot = Valiquot =

Conc(H2SO4,front) = $[\text{K} * \text{N} * \text{Vt} * (\text{Vsoln} / \text{Valiquot})] / \text{Vm}(\text{std}) =$

Cs(H2SO4,front) = $15.43 * \text{Conc}(\text{H}_2\text{SO}_4, \text{front}) =$

Cs(H2SO4,12%,front) = $\text{Cs}(\text{front}) * (12 / \% \text{CO}_2) =$

E (H2SO4,front) = $0.00857 * \text{Qstd} * \text{Cs}(\text{H}_2\text{SO}_4, \text{front}) =$

FILTER

Volume of the titrant = Vt

Volume of the solution = Vsoln =

Volume of the aliquot = Valiquot =

Conc(H2SO4,filter) = $[\text{K} * \text{N} * \text{Vt} * (\text{Vsoln} / \text{Valiquot})] / \text{Vm}(\text{std}) =$

Cs(H2SO4,filter) = $15.43 * \text{Conc}(\text{H}_2\text{SO}_4, \text{filter}) =$

Cs(H2SO4,12%,filter) = $\text{Cs}(\text{filter}) * (12 / \% \text{CO}_2) =$

E (H2SO4,filter) = $0.00857 * \text{Qstd} * \text{Cs}(\text{H}_2\text{SO}_4, \text{filter}) =$

BACK HALF

Volume of the titrant = Vt

Volume of the solution = Vsoln =

Volume of the aliquot = Valiquot =

Conc(H2SO4,back) = $[\text{K} * \text{N} * \text{Vt} * (\text{Vsoln} / \text{Valiquot})] / \text{Vm}(\text{std}) =$

Cs(H2SO4,back) = $15.43 * \text{Conc}(\text{H}_2\text{SO}_4, \text{back}) =$

Cs(H2SO4,12%,back) = $\text{Cs}(\text{H}_2\text{SO}_4, \text{back}) * (12 / \% \text{CO}_2) =$

E (H2SO4,back) = $0.00857 * \text{Qstd} * \text{Cs}(\text{H}_2\text{SO}_4, \text{back}) =$

TOTAL SO3

Conc(H2SO4,total) = $\sum \text{Conc}(\text{H}_2\text{SO}_4, \text{location})$

Cs(H2SO4,total) = $\sum \text{Cs}(\text{H}_2\text{SO}_4, \text{location}) =$

Cs(H2SO4,12%,total) = $\sum \text{Cs}(\text{H}_2\text{SO}_4, 12\%, \text{location}) =$

E (H2SO4,total) = $\sum \text{E}(\text{H}_2\text{SO}_4, \text{location}) =$

SDAPCD	SCEC
0.00971	0.00971 equiv/liter
32.362	32.36 dscf
3246	3267 dscfm
7.81	7.81 %
15.43	15.4 grains/gram
0.00857	0.00857 lbs-min/grs-hr

98.08

** 97 g/mole

2

2 equiv/mole

49.04

48.5 grams/equiv

0	0 ml
150	150 ml
10	10 ml
0.0000000	0.0000000 grams/dscf
0.0000000	0.0000000 grains/dscf
0.0000000	0.0000000 grains/dscf
0.0000	0.0000 lbs/hr

0	0 ml
100	100 ml
10	10 ml
0.0000000	0.0000000 grams/dscf
0.0000000	0.0000000 grains/dscf
0.0000000	0.0000000 grains/dscf
0.0000	0.0000 lbs/hr

0.24	0.24 ml
280	280 ml
10	10 ml
0.0000989	0.0000978 grams/dscf
0.0015257	0.0015061 grains/dscf
0.0023442	0.0023140 grains/dscf
0.0424	0.0419 lbs/hr

0.0000989	0.0000978 grams/dscf
0.0015257	0.0015061 grains/dscf
0.0023442	0.0023140 grains/dscf
0.0424	0.0419 lbs/hr

COMMENTS:

** SCEC used an incorrect molecular weight for H2SO4, and this gave incorrect values for all the subsequent numbers that SCEC generated in its final report.

The District will use the numbers generated by the District's spreadsheet, because these values are correct.

$$\text{Concentration}(\text{SO}_2) = [K * \text{Normality} * V_{\text{titrant}} * (V_{\text{solution}} / V_{\text{aliquot}})] / V_{\text{m}} - (\text{std})$$

CALCULATIONS:

SCCELLANEEOUS DATA

N = Normality =

Vmstd =

Qstd =

%CO₂ =

15.43 grains = 1 gram

7000grains=1lb, 60min=1hr; 60min/hr/7000grains/lb=

SO₂:

MW =

equiv/mole vs. BaCl₂ =

K =

FRONT HALF

Volume of the titrant = Vt

Volume of the solution = Vsoln =

Volume of the aliquot = Valiquot =

Conc(SO₂,front) = $[K * N * V_t * (V_{\text{soln}} / V_{\text{aliquot}})] / V_{\text{m}}(\text{std}) =$

Cs(SO₂,front) = 15.43 * Conc(SO₂,front) =

Cs(SO₂,12%,front) = Cs(SO₂,front) * (12/%CO₂) =

E (SO₂,front) = 0.00857 * Qstd * Cs(SO₂,front) =

FILTER

Volume of the titrant = Vt

Volume of the solution = Vsoln =

Volume of the aliquot = Valiquot =

Conc(SO₂,filter) = $[K * N * V_t * (V_{\text{soln}} / V_{\text{aliquot}})] / V_{\text{m}}(\text{std}) =$

Cs(SO₂,filter) = 15.43 * Conc(SO₂,filter) =

Cs(SO₂,12%,filter) = Cs(SO₂,filter) * (12/%CO₂) =

E (SO₂,filter) = 0.00857 * Qstd * Cs(SO₂,filter) =

BACK HALF

Volume of the titrant = Vt

Volume of the solution = Vsoln =

Volume of the aliquot = Valiquot =

Conc(SO₂,back) = $[K * N * V_t * (V_{\text{soln}} / V_{\text{aliquot}})] / V_{\text{m}}(\text{std}) =$

Cs(SO₂,back) = 15.43 * Conc(SO₂,back) =

Cs(SO₂,12%,back) = Cs(SO₂,back) * (12/%CO₂) =

E (SO₂,back) = 0.00857 * Qstd * Cs(SO₂,back) =

TOTAL SO₂

Conc(SO₂,total) = $\sum \text{Conc}(\text{SO}_2, \text{location})$

Cs(SO₂,total) = $\sum \text{Cs}(\text{SO}_2, \text{location}) =$

Cs(SO₂,12%,total) = $\sum \text{Cs}(\text{SO}_2, 12\%, \text{location}) =$

E (SO₂,total) = $\sum \text{E}(\text{SO}_2, \text{location}) =$

SDAPCD

SCEC

0.00971
32.362
3246
7.81

15.43

0.00857

64.06

2

32.03

0
150
10

0.0000000

0.0000000

0.0000000

0.0000

0
100
10

0.0000000

0.0000000

0.0000000

0.0000

0.24
280
10

0.0000646

0.0009965

0.0015311

0.0277

0.0000646

0.0009965

0.0015311

0.0277

0.00971 equiv/liter

32.36 dscf

3267 dscfm

7.81 %

15.4 grains/gram

0.00857 lbs-min/grs-hr

not done g/mole

not done equiv/mole

not done grams/equiv

not done ml

not done ml

not done ml

not done grams/dscf

not done grains/dscf

not done grains/dscf

not done lbs/hr

not done ml

not done ml

not done ml

not done grams/dscf

not done grains/dscf

not done grains/dscf

not done lbs/hr

not done ml

not done ml

not done ml

not done grams/dscf

not done grains/dscf

not done grains/dscf

not done lbs/hr

not done grams/dscf

not done grains/dscf

not done grains/dscf

not done lbs/hr

COMMENTS:

SCEC did not calculate the contribution due to SO₂; so, the District will use the values generated by the District's spreadsheet.

COMPANY: ARIZONA STREET
 DATE: 3/30/92
 UNIT: FLARE
 REPORT #: T1482-1

RUN #3
 @ 68°F
 EPA METHOD 5/8

PARTICULATE RESULTS:	net mg	gr/dscf	gr/scf	gr/dscf @ 12% CO2	lbs/hr
Probe & Nozzle:	5.3	0.002522	0.002304	0.003875	0.07
Filter:	2.6	0.001237	0.001130	0.001901	0.03
Condensables:	1.26	0.000599	0.000547	0.000921	0.02
Total:	9.16	0.004359	0.003982	0.006697	0.12

N BaCl = 0.00971

SULFATE RESULTS:	Vol aliq	Vt	gr/dscf	gr/scf	gr/dscf @ 12% CO2	lbs/hr
Probe & Nozzle:	15	0	0	0	0	0
Filter:	10	0	0	0	0	0
Condensables:	28	0.24	0.001506	0.001375	0.002314	0.04
Total:			0.001506	0.001375	0.002314	0.04

ADDITIONAL DATA:

TIME		%O2	%CO2	%H2O	Vm(std)	SDCFM
start	finish					
1600	1700	11.7	7.81	8.65	32.36	3267

Client: COPIED @ 4:20Analyst: Report #: T-1482Test Date: 3/30/92

TITRIMETRIC ANALYSIS

Sample I.D./Run #	Total Sample (mls)	Aliquot mls	Normality	Titrant mls
N =	—			
N = 2	70	10	0.009710	0
N = 2	150	10	0.009710	0
N =	545	10	0.009710	0.08
COND #2	340	10	0.009710	0.12
COND #3	280	10	0.009710	0.24
T.H. #1	100	10	0.009710	0
#2	100	10	0.009710	0
#3	100	10	0.009710	0

COMMENTS:

NOx and CO Analysis

OFFICIAL TEST RESULTS:

GAS	TEST PPM	LIMITS (PPM)	PERFORMANCE EXCEEDANCE/NON-EXCEEDANCE
NOx	29.49	N/A	N/A
CO	0.00	N/A	N/A

TEST PARAMETERS:

PROCEDURES & CALCULATIONS:

All the procedures, calculations and equipment utilized in these tests are based on EPA NSPS guidelines and from the EPA CFR 40, July 1, 1991, parts 53-60, Method 20, except where noted in the SDAPCD QA manual for Method 20 testing.

SAMPLING & EQUIPMENT:

SCEC provided all the sampling and analysis equipment, and they were responsible for all the calibrations according to EPA guidelines.

OVERVIEW OF THE TEST:

- (1) SCEC did not perform the NO₂ converter equation correctly. The District corrected for this.
- (2) SCEC did not subtract [NO] from [NO_x].
- (3) SCEC's O₂ calibrations are high (not within +/- 2% full scale).

RUN #1: *ACCEPTED*

RUN #2: *ACCEPTED*

RUN #3: *ACCEPTED*

SUMMARY OF ALL 3 TESTS:

	NO _x		CO	
	SCEC	APCD	SCEC	APCD
RUN 1	30.46	30.54	0.00	0.00
RUN 2	28.38	28.42	0.00	0.00
RUN 3	29.40	29.50	0.00	0.00
AVERAGE	29.41	29.49	0.00	0.00

COMPANY: ARIZONA STREET
DATE: MARCH 30, 1992
UNIT: FLARE
REPORT #: T1482-1

NO2 - NOx ADJUSTMENTS

RUN #	NOX	NO ppm	NO2 ppm	% Recovery	NOx ADJUSTED VALUES	
					NO2 ppm	NOX ppm
#1	15.95	15.95	0	95.7	0.00	15.95
#2	14.58	13.75	0.83	95.7	0.87	14.62
#3	15.1	13.75	1.35	95.7	1.41	15.16
AVERAGE					0.76	15.24

CONTRACTOR TEST REPORT

SAN DIEGO AIR POLLUTION CONTROL DISTRICT
MONITORING AND TECHNICAL SERVICES
9150 CHESAPEAKE DRIVE
SAN DIEGO, CA 92123

NITROGEN OXIDES, CARBON MONOXIDE, PARTICULATE,
AND SULFUR EMISSIONS SUMMARY REPORT

SITE: Arizona Street Flare

P/O NUMBER: 56896 and 59383 JOB NO: T1482-1

TEST DATE: 3/30/92

EQUIPMENT: Arizona Street Landfill Gas Collection and Incineration System

REPORT BY: *R.P. Logan* DATE: 5/14/92
R.P. Logan - SCEC

APCD PERSONNEL: Janet Cawver/David Shina *5/13/92*

SITE PERSONNEL: Ray Purtee

APPROVED BY: _____ DATE: _____

Table 1. Summary of Results - average NO_x and CO stack emissions corrected to 3% O₂.

	TEST (ppm)	PERMIT LIMITS (ppm)	PERFORMANCE	HOURS OF TEST
NO _x	29.49	N/A	N/A	3.0
CO	0.00	N/A	N/A	3.0

* Particulate and sulfur results can be found on Page 4

TEST REFERENCE: This testing was performed in accordance with the San Diego Air Pollution Control District Method 20: "Test Procedures For The Determination of Nitrogen Oxides, Carbon Monoxide and Diluent Gases by Continuous Emission Monitoring"

P/O NUMBER: 56896 and 59383

DATE: 3/30/92

Table 2. Stack Emissions of NO_x, CO, and O₂

RUN	SCALE TIME	NO _x 0-350 PPM CORR 3% O ₂			CO 0-500 PPM CORR 3% O ₂			O ₂ 0-25%	
		CHART (div)	UNCORR (ppm)	CORR (ppm)	CHART (div)	UNCORR (ppm)	CORR (ppm)	CHART (div)	%
R1	12:30								
Avg.	13:30	6.38	15.95	30.54	0.0	0.0	0.0	46.2	11.55
PK1									
PK2									
R2	13:40								
Avg.	14:40	5.85	14.62	28.42	0.0	0.0	0.0	46.8	11.69
PK1									
PK2									
R3	14:50								
Avg.	16:00	6.06	15.16	29.50	0.0	0.0	0.0	46.8	11.70
PK1									
PK2									

Peak =

Overall = 6.10 15.24 29.49 0.0 0.0 0.0 46.6 11.65

NO_x and CO:

- The value reported is the average concentration value at 3% O₂, when:
The average pollutant concentration exceeds the permit limit, or the average value is within the permit limit and there are less than two excursions above the limit.
- The value reported is the highest excursion value at 3% O₂, when:
There are two or more excursions above the permit limit during the three subtests.
- If it has been determined that stratification exists, the average concentration values of NO_x and CO, at 3% O₂, are then reported.

Table 3. Calibration Gases

	CYLINDER	MANUFACTURER	CONCENTRATION (ppm)
NO _x	CC7297	Scott Marrin	214.2
CO	CC67219	Scott Marrin	476
O ₂	CC106786	Scott Marrin	8.40%
NO ₂	CC548	Scott Marrin	176.0

P/O NUMBER: 56896 and 59383

DATE: 3/30/92

ANALYZER CHECK LIST

	YES	NO	COMMENTS
NO_x Analyzer			
analyzer calibrated	X		
analyzer set to zero	X		
zero drift < or = 2% of span	X		
reset zero	X		
span drift < or = 2%	X		
reset span	X		
response time within limits	X		
CO Analyzer			
analyzer calibrated	X		
analyzer set to zero	X		
zero drift < or = 2% of span	X		
reset zero	X		
span drift < or = 2%	X		
reset span	X		
O₂ Analyzer			
high calibration set to 20.95%	X		
low cal. set to exhaust gas		X	Set @ 8.4% Gas
zero drift < or = 2% of span	X		
reset zero	X		
span drift < or = 2%	X		
reset span	X		
System Integrity/Leak Check			
pre-testing: performed w/NO/NO ₂	X		
post testing: performed w/NO/NO ₂	X		
System Assembly			
probe installed	X		
moisture removal trap used	X		
particulate filter used	X		
sample manifold pressure set	X		
Data Recording			
annotated	X		
electronic zero set on each pen	X		
chart speed set	X		
converter efficiency: NO ₂ to NO	X		
certificates of cal. gases	X		



SCOTT-MARRIN, INC.

6531 BOX SPRINGS BLVD. • RIVERSIDE, CA 92507
TELEPHONE (714) 653-6780 • FAX (714) 653-2430

REPORT OF ANALYSIS
EPA PROTOCOL GAS MIXTURES

SOCE01

TO:

KEITH SHANNON

SCIC

15882-1 NORTH BATAVIA

ORANGE, CA 92667-

DATE : 03/02/92

CUSTOMER ORDER NUMBER: 446

PAGE 1

COMPONENT	CONCENTRATION (v/v)	REFERENCE STANDARD	ANALYZER MAKE, MODEL, S/N, DETECTION	EXPIRATION DATE	REPLICATE ANALYSIS DATA
CYLINDER NO.: CC29002					
Carbon Dioxide	12.16 ± 0.12 %	GMIS Cylinder # CCS6263 @ 17.61 g	Varian Model 1868 S/N None Thermal Conductivity Gas Chromatography Last Cal Date: 12/06/91	08/25/93	02/25/92 12.23 % 11.99 % 12.25 % Mean: 12.16 %
Ygen	4.08 ± 0.04 %	GMIS Cylinder # CCS1219 @ 5.13 g	Varian Model 1868 S/N None Thermal Conductivity Gas Chromatography Last Cal Date: 12/10/91	08/25/93	02/25/92 4.09 % 4.08 % 4.08 % Mean: 4.08 %
CYLINDER NO.: CC106786					
Oxygen	8.40 ± 0.08 %	GMIS Cylinder # CCS2350 @ 7.37 g	Varian Model 1868 S/N None Thermal Conductivity Gas Chromatography Last Cal Date: 4/07/92	08/25/93	02/25/92 8.42 % 8.38 % 8.48 % Mean: 8.40 %
Carbon Dioxide	13.47 ± 0.13 %	GMIS Cylinder # CCS6263 @ 17.61 g	Varian Model 1868 S/N None Thermal Conductivity Gas Chromatography Last Cal Date: 12/06/91	08/25/93	02/25/92 13.42 % 13.46 % 13.53 % Mean: 13.47 %

ppm = umole/mole

% = mole-%

The above analyses were performed in accordance with EPA-1987 Traceability Protocol
1, Section 3.8.1, Procedure G1.

Analyst:

M.S. Calhoun

Approved:

J.T. Parrin

The only liability of this company for gas which fails to comply with this analysis shall be replacement or reanalysis thereof by the
company without extra cost.

STANDARD CALIBRATION GASES IN ALUMINUM CYLINDERS



SCOTT-MARRIN, INC.
2001 THIRD ST. • UNIT H • RIVERSIDE, CA 92507
TELEPHONE (714) 784-1240

RECEIVED

REPORT OF ANALYSIS
EPA PROTOCOL GAS MIXTURES

SOCE01

TO:

KEITH SHANNON
SOUTH COAST ENVIRONMENTAL CORP
1915 MCKINLEY AVE., ST. E
LA VERNE, CA 91750

DATE : 05/14/91

CUSTOMER ORDER NUMBER: 294

PAGE 1

COMPONENT		CONCENTRATION (v/v)	REFERENCE STANDARD	ANALYZER MAKE, MODEL, S/N, DETECTION	EXPIRATION DATE	REPLICATE ANALYSIS DATA	
CYLINDER NO.:		CC7297					
Nitric Oxide		214.2 ± 2.1 ppm	GVLS	Monitor Labs Model 8448		05/06/91	05/14/91
				S/N 136	11/14/92	211.2 ppm	215.3 ppm
Nitrogen, O2-Free Balance			Cylinder #	Continuous		214.9 ppm	214.4 ppm
Cylinder Pressure: 2000 psig			CC7341	Chemiluminescence		211.3 ppm	214.5 ppm
			@ 247.6 ppm	Last Cal Date: 05/01/91		Mean: 211.3 ppm	214.5 ppm

ppm = umole/mole

% = mole-%

The above analyses were performed in accordance with EPA-1987 Traceability Protocol # 1, Section 3.0.4, Procedure G1.

Analyst

B.E. Gross

Approved:

J.T. Marrin

The only liability of this company for gas which fails to comply with this analysis shall be replacement or reanalysis thereof by the company without extra cost.

STANDARD CALIBRATION GASES IN ALUMINUM CYLINDERS



SCOTT-MARRIN, INC.
2001 THIRD ST. • UNIT H • RIVERSIDE, CA 92507
TELEPHONE (714) 784-1240

RECEIVED SEP

REPORT OF ANALYSIS
EPA PROTOCOL GAS MIXTURES

SOCE01
TO: RUSS LOGAN
SOUTH COAST ENVIRONMENTAL CORP
1915 MCKINLEY AVE.
SUITE E
LAVERNE, CA 91750

DATE : 08/30/91

CUSTOMER ORDER NUMBER: 343

PAGE 1

XX					
COMPONENT	CONCENTRATION (v/v)	REFERENCE STANDARD	ANALYZER MAKE, MODEL, S/N, DETECTION	EXPIRATION DATE	REPLICATE ANALYSIS DATA
CYLINDER NO.: CC67219					
Carbon Monoxide	476 ± 5 ppm	GM13	Carle Insta Model 8000 S/N 8249	02/29/93	07/28/89 08/29/91 475 ppm 475 ppm
Nitrogen	Balance	Cylinder # CC28362	Methanation/FID		473 ppm 477 ppm
Cylinder Pressure:	2000 psig	0.496 ppm	Gas Chromatography		473 ppm 481 ppm
Last Cal Date: 07/19/91				Mean: 474 ppm	478 ppm

ppm = umole/mole

% = mole-%

The above analyses were performed in accordance with EPA-1987 Traceability Protocol # 1, Section 3.0.4, Procedure G1.

Analyst: Mark Monson
M.J. Monson

Approved: J.T. Marrin
J.T. Marrin

The only liability of this company for gas which fails to comply with this analysis shall be replacement or reanalysis thereof by the company without extra cost.

STANDARD CALIBRATION GASES IN ANALYSIS



SCOTT-MARRIN, INC.

2001 THIRD ST. • UNIT H • RIVERSIDE, CA 92507
TELEPHONE (714) 784-1240

REPORT OF ANALYSIS NIST TRACEABLE GAS MIXTURES

80CE81

TO:

LESLIE JOHNSON
SOUTH COAST ENVIRONMENTAL
1582-1 N. BATAVIA STREET
ORANGE, CA 92667-

DATE: 01/13/92

CUSTOMER ORDER NUMBER: 427

PAGE 1

CYLINDER NUMBER	COMPONENT	CONCENTRATION (v/v)	NIST TRACEABLE REFERENCE STANDARD
CC648	Nitrogen Dioxide Nitrogen	176.8 ± 1.8 ppmv Balance	SRM 2627

Post-It™ brand fax transmittal memo 7671		# of pages > 1
To: Russ Logan	From: Debbie	
Co.	Co.	
Dept.	Phone #	653 6780
Fax # (714) 252-8247	Fax #	

ppm = umole/mole

% = mole-%

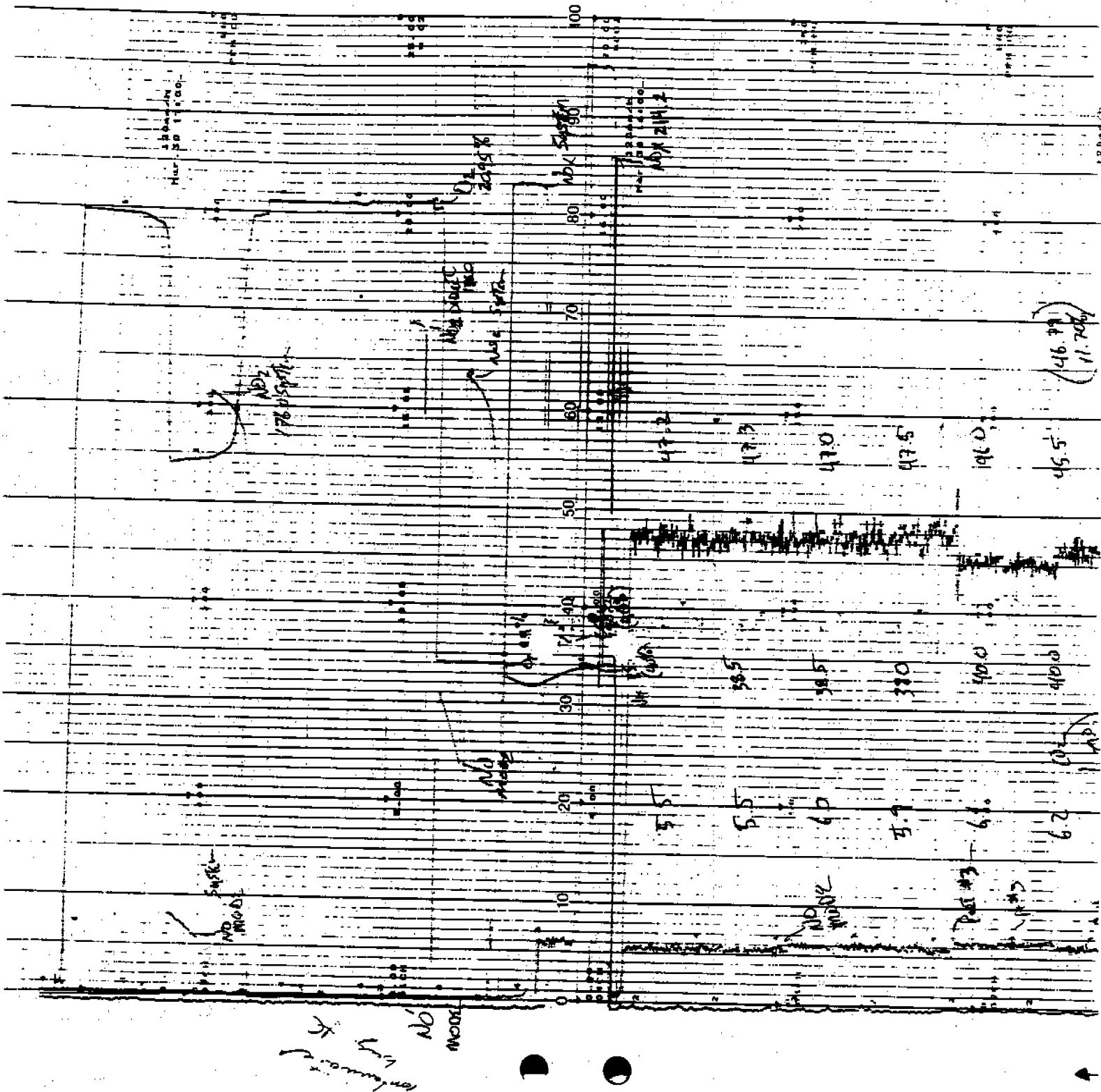
The above analysis is traceable to the National Institute of Standards and Technology by intercomparison with the reference standard listed above. Where indicated, volumetric and gravimetric reference standards are traceable thru use of our analytical balance. NIST Report No. MMAP 232.89/282491.

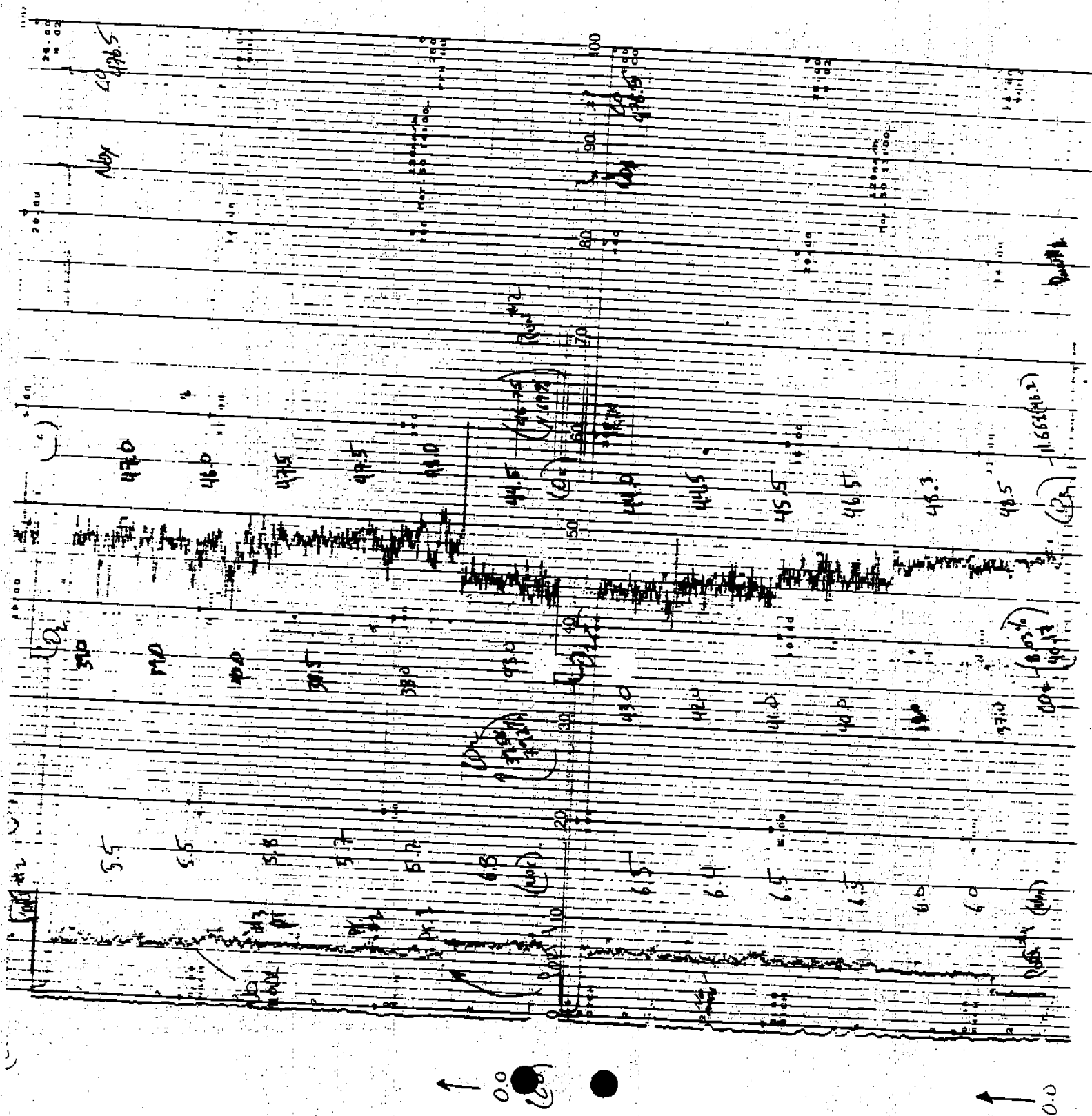
Analyst:

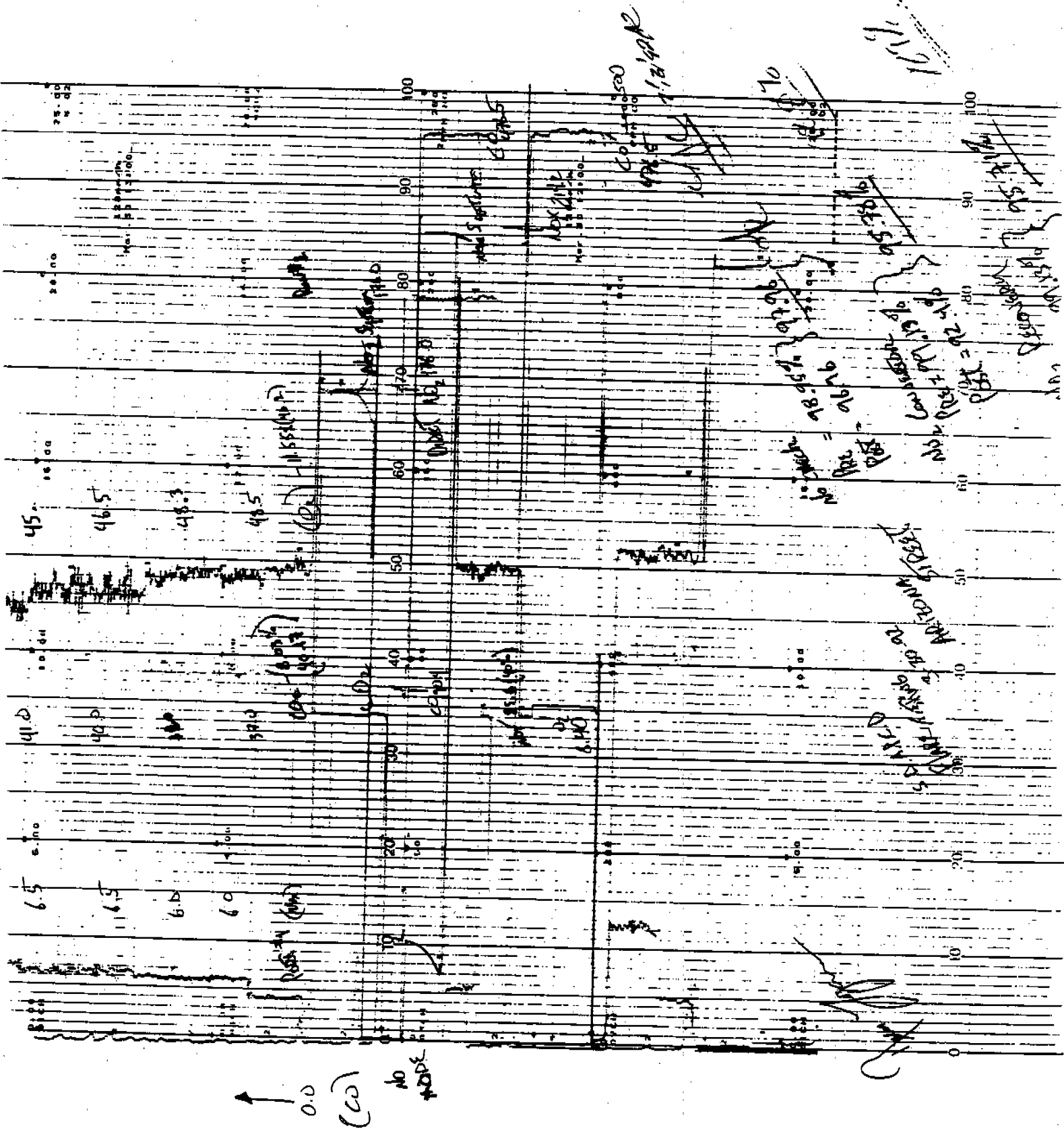
Approved:

B.E. Gross

J.T. Marrin







DISTRICT QC

①

Arizona St: Glendale J. Canyon 7/13/42

SALES

CO 0-500

O₂ 0-25%

NO_x 0-250

CALGAS

476.5 ppm = 95.30 ch div

190.0 ppm = 38.0

20.95% = 83.8

8.40% = 33.6

214.2 ppm = 85.6

85.6 = 34.2

NO₂: 176.0 ppm
= 70.4 ch div

Limit = ±2% FS
= ±2 ch div

<u>read</u>	<u>Calc</u>	<u>ACT</u>	<u>DIF</u>	<u>OK</u>	<u>ZERO</u>	<u>ACT</u>	<u>DIF</u>	<u>OK</u>
CO	96.0	95.3	0.7	✓	-1.5	0	-1.5	✓
O ₂	34.2	33.6	0.8	✓	0	0	0	✓
NO _x	85.9	85.6	0.3	✓	-1.5	0	-1.5	✓
	34.1	34.2	0.1	✓	0	0	0	✓
O	37.0	38.0	1.0	✓	-1.5	0	-1.5	✓

SALES = OK

NO SYSTEM = 85.0 ch div

85.0 / 85.9 = 99.0%

NO₂ convert en No mode 69.0

ACT = 70.4

No mode 0

69.0 / 70.4 = 98.0% 69.0

O₂ Recovery: No mode 68.0

No mode 1.0

67.0 / 69.0 = 97.1% 67.0

(No mode - not marked, appears ± 1 ch div)

SYSTEMS = OK

	ch div	=	ppm	=	at 3% O ₂	REPORT <u>ECOC</u>
N#1:	CO	0	=	0	=	0, 0, 0 *
	NO _x	6.38	=	15.95	=	6.38, 15.95, 30.54
	O ₂	46.2	=	11.55	CF = 1.910	46.2, 11.55

zona ST : QC NIZO

KLJ1 CONT
135 - 13.35

TIMES: NOx 30 min + + NO mode 10 min
CO 30 min + O₂ 30 min +

→ Sample at port # 4

→ NO STRAT YET (will do in 1, 1, 1, 2)

→ NO PEAKS

ENC₂ = 0

Gas	CAL	ACT	DIF	OK
NO	86.0	85.6	0.4	✓
CO	95.0	95.3	0.3	✓
O ₂	34.2	33.6	0.8	✓

ZERO	ACT	DIF	OK
0	0	0	✓
-5	0	-5	✓
3	0	3	✓

CALS = OK

SCEC REPORT

RUN #2:

340 - 14:47

ch dir = ppm = at 3% O₂
CO = 0 = 0 = 0

NOx = 5.85 = 14.63 = 23.38

O₂ = 46.8 = 11.69 CF = 1.94

NO₂ = 0

ch dir = ppm = at 3% O₂

0 = 0 = 0

5.85 = 14.62 = 23.42

46.8 = 11.61

0

→ STRAT CR DONE . 4 points

O₂ AVE = 46.8

5% of AVE = 2.34 ch dir

lowest O₂ = 44.5

46.8 - 2.34 = 44.46

so NO STRAT

#4 O₂ level = falls

just w/in limits of STRATIFICATION

Times: NOx 30 min +

NO mode = 10 min +

CO 30 min +

O₂ 30 min +

PEAKS: NOx

AS	CAL	ACT	DIF	OK
NO	85.4	85.6	0.6	✓
CO	95.0	95.3	0.3	✓
O ₂	34.2	33.6	0.8	✓

ZERO	ACT	DIF	OK
0	0	0	✓
-5	0	-5	✓
5	0	5	✓

CALS = OK

Arizona St. GC m20

SCC REPORT

RUN #3

14.50 - 16.00

ch div = ppm - @ 32002
 NOx: 6.06 = 18.15 = 29.40
 CO 0 = 0 = 0
 O2 46.8 = 11.70 CF = 1.94

ch div = ppm - @ 32002
 6.06 = 18.15 = 29.52
 0 = 0 = 0
 46.8 = 11.70

TIMES / (NOx, NO, CO, O2) = OK

STRAT CK = DONE

Ave O2 = 46.8 5% = 2.34

46.8 - 2.34 = 44.46

lowest O2 = 45.5

PEAKS: NONE [NO2] = 0

GAS	CAL	ACT	DIF	OK	ZERO	ACT	DIF	OK
NO	85.9	85.6	0.3	✓	-1	0	-1	✓
O2	34.1	33.6	0.5	✓	.5	0	.5	✓
	95.0	95.3	0.3	✓	-1.5	0	-1.5	✓
O2	81.0	83.8	2.8	✗	.5	0	.5	✓

CALS = OK

* O2 for 20.95 low by 0.8% FS. Questionable humidity on O2.

O2 data = Cals at 8.49% O2 - near emissions of 21.1% O2. Therefore will accept data.

NO SYSTEM = 83.0 ch div
 $83.0 / 25 = 96.6\%$

NO2 converter: NOx mode 68.9
 (DIRECT) No mode: 0
 $68.9 / 70.4 = 97.9\%$ 68.9

O2 Recovery: NOx mode: 61.3

No mode: 5.8

55.5

$55.5 / 68.9 = 80.6\%$

Arizona St: GC MZ4

SUMMARY:

SCFC

SYSTEMS: NO SYSTEM = OK AVE = $\frac{96.6 + 99.0}{2} = \underline{97.8\%}$ 97.9

NO₂ conversion = OK AVE = $\frac{97.9 + 99.01}{2} = \underline{98.45\%}$ 95.78

NO₂ RECOVERY = OK AVE = $\frac{97.10 + 80.6\%}{2} = \underline{88.9\%}$ 95.71

SCFC post NO₂ conversion (176 ppm NO₂ = 70.4 ch div = ACT)
NO_x = 68.9 ch div $68.9 / 70.4 = \underline{97.9\%}$
NO = 0 ch div
NO₂ = 68.9 ch div
SCFC $\Rightarrow \underline{92.4\%}$ $\rightarrow$ calc incorrectly

* SCFC = Does not subtract [NO₂] from [NO_x] in order to get [NO₂] through syst & $\therefore$ NO₂ recovery.
 $\therefore$ SCFC NO₂ recovery is higher.

NO₂ CHL DRIFTS: NO DRIFTS - DATA CORRS NOT NEEDED

PT CALS: OK for NO_x & CO

$\rightarrow$ O₂ CAL (HIGH) NOT w/in 2% FS

However, CALS @ emission level & data is accepted.

TRAT CK: Done, NO STRAT DETERMINED

NO₂: [NO₂] = 0 - 110 - 110 - 110 - 110 - 110 - 110 - 110 - 110 - 110

Arizona St. GC M20

$\gamma_{NO_2} = 1$ all runs $\therefore$

DATA SUMMARY

	NOx (G/L) / ppm	3% O ₂	CO	O ₂	CF		
<u>R#1</u> (GC)	6.38	15.95	30.46	Ø	46.2	11.55	1.9096
(SEC)	6.38	15.95	30.54	Ø	46.2	11.55	1.915
<u>R#2</u> (GC)	5.85	14.63	28.38	Ø	46.8	11.69	1.938
(SEC)	5.85	14.62	28.43	Ø	46.8	11.69	1.944
<u>R#3</u> (GC)	6.06	15.15	29.40	Ø	46.8	11.70	1.941
(SEC)	6.06	15.16	29.50	Ø	46.8	11.70	1.946

$$\Sigma CF = \frac{20.95 - 3}{20.95 - O_2\%}$$

$$CORR NO_x = NO_x \cdot CF \rightarrow \text{TO FIND}$$

$$\text{SEC CF} = \frac{CORR NO_x}{NO_x} \quad CF \text{ SEC USED}$$

GC AVE NO_x = 29.41 @ 3% O₂

SEC AVE NO_x = 29.49 @ 3% O₂

Diffs could be due to round off error in determining O₂ correction factors. The final ave b/w GC & SEC is .08% $\therefore$ will accept data.

Test Witness - Runs #1 - 3 GC Analysis

TEST PARAMETERS:

PROCEDURES:

The procedures and equipment utilized in these tests are based on EPA NSPS guidelines and from the EPA CFR 40, Method 18.

CALCULATIONS:

All calculations are based on the EPA CFR 40, July 1, 1991, Parts 53-60, Method 18.

GAS SAMPLING:

SCEC performed all the field testing. Their procedures are as follows:

A pressurized container was placed at the gas inlet BEFORE the flare. The container was opened after the flare reached a steady state. Once at a steady state, the container drew in the landfill gas for 25 minutes. After 25 minutes, the container was shut off, labeled and shipped to Performance Analytical Inc. The outlet monitoring was run concurrently and parallel to the particulate sampling (AFTER the flare). An EPA Method 20 probe with teflon tubing connecting the probe to the pressurized container was used. The pressurized container was opened and allowed to draw in the outlet gas for 25 minutes. The container was then shut off, labeled and shipped to Performance Analytical Inc.

ANALYSES:

All analyses were performed by Performance Analytical Inc.

EQUIPMENT:

All testing and analysis equipment was calibrated according to EPA guidelines and performed by Performance Analytical Inc.

OVERVIEW OF THE TEST:

RUN #1: INLET: Accepted
OUTLET: Accepted

RUN #2: INLET: Accepted
OUTLET: Accepted

RUN #3: INLET: Accepted
OUTLET: Accepted

	INLET #1		OUTLET #1	
	RESULT (PPM)	DET. LIMIT (PPM)	RESULT (PPM)	DET. LIMIT (PPM)
C1 as Methane	400000	150	76	2.5
C2 as Ethane	ND	150	ND	2.5
C3 as n-Propane	ND	120	ND	2.0
C4 as n-Butane	ND	90	ND	1.5
C5 as Pentane	ND	60	ND	1.0
C6 as n-Hexane	ND	60	ND	1.0
C7 as n-Heptane	ND	60	ND	1.0
C8 as n-Octane	ND	60	ND	1.0
C9 as n-Nonane	ND	60	ND	1.0
> C9 as n-Nonane	ND	60	ND	1.0
	RESULT (PPB)	DET. LIMIT (PPB)	RESULT (PPB)	DET. LIMIT (PPB)
	RESULT (PPB)	DET. LIMIT (PPB)	RESULT (PPB)	DET. LIMIT (PPB)
Vinyl Chloride	890	240	ND	9.9
Methylene Chloride	270	170	6.5	TR 7.3
Chloroform	ND	120	ND	5.2
1,2-Dichloroethane	ND	150	ND	6.2
1,1,1-Trichloroethane	450	110	ND	4.8
Benzene	180	TR 190	1.6	7.8
Carbon Tetrachloride	ND	97	ND	4.0
Trichloroethene	710	110	ND	4.7
1,2-Dibromoethane	ND	75	ND	3.3
Tetrachloroethene	1200	89	ND	3.7

	INLET #2		OUTLET #2	
	RESULT (PPM)	DET. LIMIT (PPM)	RESULT (PPM)	DET. LIMIT (PPM)
C1 as Methane	120000	25	ND	4.0
C2 as Ethane	ND	25	ND	4.0
C3 as n-Propane	ND	20	ND	3.2
C4 as n-Butane	ND	15	ND	2.4
C5 as Pentane	ND	10	ND	1.6
C6 as n-Hexane	ND	10	ND	1.6
C7 as n-Heptane	ND	10	ND	1.6
C8 as n-Octane	ND	10	ND	1.6
C9 as n-Nonane	ND	10	ND	1.6
> C9 as n-Nonane	ND	10	ND	1.6
	RESULT (PPB)	DET. LIMIT (PPB)	RESULT (PPB)	DET. LIMIT (PPB)
	RESULT (PPB)	DET. LIMIT (PPB)	RESULT (PPB)	DET. LIMIT (PPB)
Vinyl Chloride	1110	30	ND	14.0
Methylene Chloride	170	29	ND	12.0
Chloroform	ND	21	ND	8.3
1,2-Dichloroethane	ND	25	ND	10.0
1,1,1-Trichloroethane	62	18	ND	7.4
Benzene	200	31	ND	13.0
Carbon Tetrachloride	ND	16	ND	6.4
Trichloroethene	750	19	ND	7.5
1,2-Dibromoethane	ND	13	ND	5.2
Tetrachloroethene	810	15	ND	6.0

	INLET #3		OUTLET #3	
	RESULT (PPM)	DET. LIMIT (PPM)	RESULT (PPM)	DET. LIMIT (PPM)
C1 as Methane	850000	180	ND	4.5
C2 as Ethane	ND	180	ND	4.5
C3 as n-Propane	ND	140	ND	3.6
C4 as n-Butane	ND	110	ND	2.7
C5 as Pentane	ND	70	ND	1.8
C6 as n-Hexane	ND	70	ND	1.8
C7 as n-Heptane	ND	70	ND	1.8
C8 as n-Octane	ND	70	ND	1.8
C9 as n-Nonane	ND	70	ND	1.8
> C9 as n-Nonane	ND	70	ND	1.8
	RESULT (PPB)	DET. LIMIT (PPB)	RESULT (PPB)	DET. LIMIT (PPB)
	RESULT (PPB)	DET. LIMIT (PPB)	RESULT (PPB)	DET. LIMIT (PPB)
Vinyl Chloride	910	280	ND	18.0
Methylene Chloride	470	200	ND	13.0
Chloroform	ND	150	ND	9.3
1,2-Dichloroethane	ND	170	ND	11.0
1,1,1-Trichloroethane	880	130	ND	8.3
Benzene	170	TR 220	ND	14.0
Carbon Tetrachloride	ND	110	ND	7.2
Trichloroethene	740	130	ND	8.5
1,2-Dibromoethane	ND	92	ND	5.9
Tetrachloroethene	1600	100	ND	6.7

	AVERAGE INLET		AVERAGE OUTLET	
	RESULT (PPM)	DET. LIMIT (PPM)	RESULT (PPM)	DET. LIMIT (PPM)
C1 as Methane	390000	118	25	3.7
C2 as Ethane	ND	118	ND	3.7
C3 as n-Propane	ND	93	ND	2.9
C4 as n-Butane	ND	72	ND	2.2
C5 as Pentane	ND	47	ND	1.5
C6 as n-Hexane	ND	47	ND	1.5
C7 as n-Heptane	ND	47	ND	1.5
C8 as n-Octane	ND	47	ND	1.5
C9 as n-Nonane	ND	47	ND	1.5
> C9 as n-Nonane	ND	47	ND	1.5
	RESULT (PPB)	DET. LIMIT (PPB)	RESULT (PPB)	DET. LIMIT (PPB)
	RESULT (PPB)	DET. LIMIT (PPB)	RESULT (PPB)	DET. LIMIT (PPB)
Vinyl Chloride	970	186	ND	14.6
Methylene Chloride	303	133	2	10.6
Chloroform	ND	97	ND	7.6
1,2-Dichloroethane	ND	115	ND	9.1
1,1,1-Trichloroethane	464	86	ND	6.8
Benzene	180	147	8	11.8
Carbon Tetrachloride	ND	74	ND	5.9
Trichloroethene	733	66	ND	6.9
1,2-Dibromoethane	ND	61	ND	4.8
Tetrachloroethene	1203	68	ND	5.6

LEGEND

ND= Not Detected

TR= Trace Level (below the indicated detection limit)

SAMPLE HISTORY

SAMPLES 1-3 INLET & OUTLET

Samples 1-3 INLET and OUTLET were taken on 3/30/92.

received on 4/2/92.

analyzed on 4/10/92.

GAS CHROMATOGRAPHY RESULTS



Performance Analytical Inc.
Environmental Testing and Consulting

File

PERFORMANCE ANALYTICAL INC.

RESULTS OF ANALYSIS

Client: San Diego Air Pollution Control District

Client Sample ID: Inlet #1 (03/30/92) (1:30)

PAI Sample ID: 9201463

Test Code: EPA-18
Analyst: Ku-Jih Chen
Instrument ID: HP5890/FID #4
Verified by: Michael Taday

Matrix: Summa Canister
Date Received: 04/02/92
Date Analyzed: 04/10/92
Volume Analyzed: 0.050 ml
 $P_i = -11.4$ $P_f = +4.0$ $DF = 5.67$

COMPOUND	RESULT (PPM)	DETECTION LIMIT (PPM)
C1 as Methane	400000	150
C2 as Ethane	ND	150
C3 as n-Propane	ND	120
C4 as n-Butane	ND	90
C5 as Pentane	ND	60
C6 as n-Hexane	ND	60
C7 as n-Heptane	ND	60
C8 as n-Octane	ND	60
C9 as n-Nonane	ND	60
> C9 as n-Nonane	ND	60

ND = Not Detected TR = Trace Level - Below Indicated Detection Limit



Performance Analytical Inc.
Environmental Testing and Consulting

PERFORMANCE ANALYTICAL INC.

RESULTS OF ANALYSIS

Client: San Diego Air Pollution Control District

Client Sample ID: Outlet #1 (03/30/92) (4:00)

PAI Sample ID: 9201466

Test Code: EPA-18
Analyst: Ku-Jih Chen
Instrument ID: HP5890/FID #4
Verified by: Michael Tuday

Matrix: Summa Canister
Date Received: 04/02/92
Date Analyzed: 04/10/92
Volume Analyzed: 2.5 ml
 $P_i = -10.6$ $P_f = +4.0$ $DF = 4.56$

COMPOUND	RESULT (PPM)	DETECTION LIMIT (PPM)
C1 as Methane	76	2.5
C2 as Ethane	ND	2.5
C3 as n-Propane	ND	2.0
C4 as n-Butane	ND	1.5
C5 as Pentane	ND	1.0
C6 as n-Hexane	ND	1.0
C7 as n-Heptane	ND	1.0
C8 as n-Octane	ND	1.0
C9 as n-Nonane	ND	1.0
> C9 as n-Nonane	ND	1.0

ND = Not Detected TR = Trace Level - Below Indicated Detection Limit



Performance Analytical Inc.
Environmental Testing and Consulting

PERFORMANCE ANALYTICAL INC.

RESULTS OF ANALYSIS

Client: San Diego Air Pollution Control District

Client Sample ID: Inlet #1 (03/30/92) (1:30)

PAI Sample ID: 9201463

Test Code: GC/MS EPA TO-14
Analyst: Chris Parnell
Instrument ID: Finnigan 4500C/Tekmar 5010
Verified by: Michael Tuday

Matrix: Summa Canister
Date Received: 04/02/92
Date Analyzed: 04/08/92
Volume Analyzed: 0.050 Liter
 $P_1 = -11.4$ $P_2 = +4.0$ $DF = 5.67$

CAS #	COMPOUND	RESULT (UG/M ³)	DETECTION LIMIT (UG/M ³)	RESULT (PPB)	DETECTION LIMIT (PPB)
75-01-4	VINYL CHLORIDE	2300	600	890	240
75-09-2	METHYLENE CHLORIDE	920	600	270	170
67-66-3	CHLOROFORM	ND	600	ND	120
107-06-2	1,2-DICHLOROETHANE	ND	600	ND	150
71-55-6	1,1,1-TRICHLOROETHANE	2400	600	450	110
71-43-2	BENZENE	570 TR	600	180 TR	190
56-23-5	CARBON TETRACHLORIDE	ND	600	ND	97
79-01-6	TRICHLOROETHENE	3800	600	710	110
106-93-4	1,2-DIBROMOETHANE	ND	600	ND	78
127-18-4	TETRACHLOROETHENE	7800	600	1200	89

ND = Not Detected TR = Trace Level - Below Indicated Detection Limit

450 - in

< 4.6 - out



Performance Analytical Inc.
Environmental Testing and Consulting

PERFORMANCE ANALYTICAL INC.

RESULTS OF ANALYSIS

Client: San Diego Air Pollution Control District

Client Sample ID: Outlet #1 (03/30/92) (4:00)

PAI Sample ID: 9201466

Test Code: GC/MS EPA TO-14
Analyst: Kathleen Aguilera
Instrument ID: Finnigan 4500C/Tekmar 5010
Verified by: Michael Tудay

Matrix: Summa Canister
Date Received: 04/02/92
Date Analyzed: 04/07/92
Volume Analyzed: 1.00 Liter
 $P_1 = -10.6$ $P_2 = +4.0$ $DF = 4.56$

CAS #	COMPOUND	RESULT (UG/M ³)	DETECTION LIMIT (UG/M ³)	RESULT (PPB)	DETECTION LIMIT (PPB)
75-01-4	VINYL CHLORIDE	ND	25	ND	9.9
75-09-2	METHYLENE CHLORIDE	22 TR	25	6.5 TR	7.3
67-66-3	CHLOROFORM	ND	25	ND	5.2
107-06-2	1,2-DICHLOROETHANE	ND	25	ND	6.2
71-55-6	1,1,1-TRICHLOROETHANE	ND	25	ND	4.6
71-43-2	BENZENE	ND	25	ND	7.8
56-23-5	CARBON TETRACHLORIDE	ND	25	ND	4.0
79-01-6	TRICHLOROETHENE	ND	25	ND	4.7
106-93-4	1,2-DIBROMOETHANE	ND	25	ND	3.3
127-18-4	TETRACHLOROETHENE	ND	25	ND	3.7

ND = Not Detected TR = Trace Level - Below Indicated Detection Limit



Performance Analytical Inc.
Environmental Testing and Consulting

PERFORMANCE ANALYTICAL INC.

RESULTS OF ANALYSIS

Client: San Diego Air Pollution Control District

Client Sample ID: Inlet #2 (03/30/92) (2:15)

PAI Sample ID: 9201464

Test Code: EPA-18
Analyst: Ku-Jih Chen
Instrument ID: HP5890/FID #4
Verified by: Michael Tuday

Matrix: Summa Canister
Date Received: 04/02/92
Date Analyzed: 04/10/92
Volume Analyzed: 0.050 ml
 $P_i = -2.1$ $P_f = +4.0$ $DF = 1.48$

COMPOUND	RESULT (PPM)	DETECTION LIMIT (PPM)
C1 as Methane	120000	25
C2 as Ethane	ND	25
C3 as n-Propane	ND	20
C4 as n-Butane	ND	15
C5 as Pentane	ND	10
C6 as n-Hexane	ND	10
C7 as n-Heptane	ND	10
C8 as n-Octane	ND	10
C9 as n-Nonane	ND	10
> C9 as n-Nonane	ND	10

ND = Not Detected TR = Trace Level - Below Indicated Detection Limit



Performance Analytical Inc.
Environmental Testing and Consulting

PERFORMANCE ANALYTICAL INC.

RESULTS OF ANALYSIS

Client: San Diego Air Pollution Control District

Client Sample ID: Outlet #2 (03/30/92) (4:30)

PAI Sample ID: 9201467

Test Code: EPA 18
Analyst: Ku-Jih Chen
Instrument ID: HP5890/FID #4
Verified by: Michael Taday

Matrix: Summa Canister
Date Received: 04/02/92
Date Analyzed: 04/10/92
Volume Analyzed: 2.5 ml
 $P_1 = -12.3$ $P_2 = +4.0$ $DF = 7.79$

COMPOUND	RESULT. (PPM)	DETECTION LIMIT (PPM)
C1 as Methane	ND	4.0
C2 as Ethane	ND	4.0
C3 as n-Propane	ND	3.2
C4 as n-Butane	ND	2.4
C5 as Pentane	ND	1.6
C6 as n-Hexane	ND	1.6
C7 as n-Heptane	ND	1.6
C8 as n-Octane	ND	1.6
C9 as n-Nonane	ND	1.6
> C9 as n-Nonane	ND	1.6

ND = Not Detected TR = Trace Level - Below Indicated Detection Limit



Performance Analytical Inc.
Environmental Testing and Consulting

PERFORMANCE ANALYTICAL INC.

RESULTS OF ANALYSIS

Client: San Diego Air Pollution Control District

Client Sample ID: Inlet #2 (03/30/92) (2:15)

PAI Sample ID: 9201464

Test Code: GC/MS EPA TO-14
Analyst: Chris Parnell
Instrument ID: Finnigan 4500C/Tekmar 5010
Verified by: Michael Tuday

Matrix: Summa Canister
Date Received: 04/02/92
Date Analyzed: 04/08/92
Volume Analyzed: 0.050 Liter
 $P_1 = -2.1$ $P_2 = +4.0$ $DF = 1.48$

CAS #	COMPOUND	RESULT (UG/M ³)	DETECTION LIMIT (UG/M ³)	RESULT (PPB)	DETECTION LIMIT (PPB)
75-01-4	VINYL CHLORIDE	2900	100	1100	39
75-09-2	METHYLENE CHLORIDE	590	100	170	29
67-66-3	CHLOROFORM	ND	100	ND	21
107-06-2	1,2-DICHLOROETHANE	ND	100	ND	25
71-55-6	1,1,1-TRICHLOROETHANE	340	100	62	19
71-43-2	BENZENE	630	100	200	31
56-23-5	CARBON TETRACHLORIDE	ND	100	ND	16
79-01-6	TRICHLOROETHENE	4000	100	750	19
106-93-4	1,2-DIBROMOETHANE	ND	100	ND	13
127-18-4	TETRACHLOROETHENE	5500	100	810	15

ND = Not Detected TR = Trace Level - Below Indicated Detection Limit

$$\begin{aligned} \text{In} &= \frac{450 + 62}{2} = 256 / 1000 = .256 \\ \text{out} &= \frac{20.6 + 14.5}{2} = 6.1 / 2000 = .003 \end{aligned}$$



Performance Analytical Inc.
Environmental Testing and Consulting

PERFORMANCE ANALYTICAL INC.

RESULTS OF ANALYSIS

Client: San Diego Air Pollution Control District

Client Sample ID: Outlet #2 (03/30/92) (4:30)

PAI Sample ID: 9201467

Test Code: GC/MS EPA TO-14
Analyst: Kathleen Aguilera
Instrument ID: Finnigan 4500C/Tekmar 5010
Verified by: Michael Tuday

Matrix: Summa Canister
Date Received: 04/02/92
Date Analyzed: 04/07/92
Volume Analyzed: 1.00 Liter
 $P_i = -12.3$ $P_f = +4.0$ $DF = 7.79$

CAS #	COMPOUND	RESULT (UG/M ³)	DETECTION LIMIT (UG/M ³)	RESULT (PPB)	DETECTION LIMIT (PPB)
75-01-4	VINYL CHLORIDE	ND	40	ND	16
75-09-2	METHYLENE CHLORIDE	ND	40	ND	12
67-66-3	CHLOROFORM	ND	40	ND	8.3
107-06-2	1,2-DICHLOROETHANE	ND	40	ND	10
71-55-6	1,1,1-TRICHLOROETHANE	ND	40	ND	7.4
71-43-2	BENZENE	ND	40	ND	13
56-23-5	CARBON TETRACHLORIDE	ND	40	ND	6.4
79-01-6	TRICHLOROETHENE	ND	40	ND	7.5
106-93-4	1,2-DIBROMOETHANE	ND	40	ND	5.2
127-18-4	TETRACHLOROETHENE	ND	40	ND	6.0

ND = Not Detected TR = Trace Level - Below Indicated Detection Limit

outlet
B
13/2001.0065



Performance Analytical Inc.
Environmental Testing and Consulting

PERFORMANCE ANALYTICAL INC.

RESULTS OF ANALYSIS

Client: San Diego Air Pollution Control District

Client Sample ID: Inlet #3 (03/30/92) (3:00)

PAI Sample ID: 9201465

Test Code: EPA-18
Analyst: Ku-Jih Chen
Instrument ID: HP5890/FID #4
Verified by: Michael Tудay

Matrix: Summa Canister
Date Received: 04/02/92
Date Analyzed: 04/10/92
Volume Analyzed: 0.050 ml
 $P_i = -12.2$ $P_f = +4.0$ $DF = 7.48$

COMPOUND	RESULT (PPM)	DETECTION LIMIT (PPM)
C1 as Methane	650000	180
C2 as Ethane	ND	180
C3 as n-Propane	ND	140
C4 as n-Butane	ND	110
C5 as Pentane	ND	70
C6 as n-Hexane	ND	70
C7 as n-Heptane	ND	70
C8 as n-Octane	ND	70
C9 as n-Nonane	ND	70
> C9 as n-Nonane	ND	70

ND = Not Detected TR = Trace Level - Below Indicated Detection Limit



Performance Analytical Inc.
Environmental Testing and Consulting

PERFORMANCE ANALYTICAL INC.

RESULTS OF ANALYSIS

Client: San Diego Air Pollution Control District

Client Sample ID: Outlet #3 (03/30/92) (5:00)

PAI Sample ID: 9201468

Test Code: EPA 18
Analyst: Ku-Jih Chen
Instrument ID: HP5890/FID #4
Verified by: Michael Tuday

Matrix: Summa Canister
Date Received: 04/02/92
Date Analyzed: 04/10/92
Volume Analyzed: 2.5 ml
 $P_i = -12.5$ $P_f = +4.0$ $DF = 8.50$

COMPOUND	RESULT . (PPM)	DETECTION LIMIT (PPM)
C1 as Methane	ND	4.5
C2 as Ethane	ND	4.5
C3 as n-Propane	ND	3.6
C4 as n-Butane	ND	2.7
C5 as Pentane	ND	1.8
C6 as n-Hexane	ND	1.8
C7 as n-Heptane	ND	1.8
C8 as n-Octane	ND	1.8
C9 as n-Nonane	ND	1.8
> C9 as n-Nonane	ND	1.8

ND = Not Detected TR = Trace Level - Below Indicated Detection Limit



Performance Analytical Inc.
Environmental Testing and Consulting

PERFORMANCE ANALYTICAL INC.

RESULTS OF ANALYSIS

Client: San Diego Air Pollution Control District

Client Sample ID: Inlet #3 (03/30/92) (3:00)

PAI Sample ID: 9201465

Test Code: GC/MS EPA TO-14
Analyst: Chris Parnell
Instrument ID: Finnigan 4500C/Tekmar 5010
Verified by: Michael Taday

Matrix: Summa Canister
Date Received: 04/02/92
Date Analyzed: 04/08/92
Volume Analyzed: 0.050 Liter
 $P_i = -12.2$ $P_f = +4.0$ $DF = 7.48$

CAS #	COMPOUND	RESULT (UG/M ³)	DETECTION LIMIT (UG/M ³)	RESULT (PPB)	DETECTION LIMIT (PPB)
75-01-4	VINYL CHLORIDE	2300	700	910	280
75-09-2	METHYLENE CHLORIDE	1600	700	470	200
67-66-3	CHLOROFORM	ND	700	ND	150
107-06-2	1,2-DICHLOROETHANE	ND	700	ND	170
71-55-6	1,1,1-TRICHLOROETHANE	4700	700	880	130
71-43-2	BENZENE	550 TR	700	170 TR	220
56-23-5	CARBON TETRACHLORIDE	ND	700	ND	110
79-01-6	TRICHLOROETHENE	3900	700	740	130
106-93-4	1,2-DIBROMOETHANE	ND	700	ND	92
127-18-4	TETRACHLOROETHENE	11000	700	1600	100

ND = Not Detected TR = Trace Level - Below Indicated Detection Limit



Performance Analytical Inc.
Environmental Testing and Consulting

PERFORMANCE ANALYTICAL INC.

RESULTS OF ANALYSIS

Client: San Diego Air Pollution Control District

Client Sample ID: Outlet #3 (03/30/92) (5:00)

PAI Sample ID: 9201468

Test Code: GC/MS EPA TO-14
Analyst: Kathleen Aguilera
Instrument ID: Finnigan 4500C/Tekmar 5010
Verified by: Michael Tuday

Matrix: Summa Canister
Date Received: 04/02/92
Date Analyzed: 04/07/92
Volume Analyzed: 1.00 Liter
 $P_i = -12.5$ $P_f = +4.0$ $DF = 8.50$

CAS #	COMPOUND	RESULT (UG/M ³)	DETECTION LIMIT (UG/M ³)	RESULT (PPB)	DETECTION LIMIT (PPB)
75-01-4	VINYL CHLORIDE	ND	45	ND	18
75-09-2	METHYLENE CHLORIDE	ND	45	ND	13
67-66-3	CHLOROFORM	ND	45	ND	9.3
107-06-2	1,2-DICHLOROETHANE	ND	45	ND	11
71-55-6	1,1,1-TRICHLOROETHANE	ND	45	ND	8.3
71-43-2	BENZENE	ND	45	ND	14
56-23-5	CARBON TETRACHLORIDE	ND	45	ND	7.2
79-01-6	TRICHLOROETHENE	ND	45	ND	8.5
106-93-4	1,2-DIBROMOETHANE	ND	45	ND	5.9
127-18-4	TETRACHLOROETHENE	ND	45	ND	6.7

ND = Not Detected TR = Trace Level - Below Indicated Detection Limit



Performance Analytical Inc.
Environmental Testing and Consulting

Beil
2-1-92 #2 10:00 AM

LABORATORY REPORT

Client: SAN DIEGO AIR POLLUTION CONTROL DISTRICT
Address: 9150 Chesapeake Drive
San Diego, CA 92123
Contact: Ms. Judy Lake
Client Project: Arizona Street & Beil Jr. High School
Date of Report: 04/21/92
Date Received: 04/02/92
PAI Project No: 4060,4061
Purchase Order: Verbal

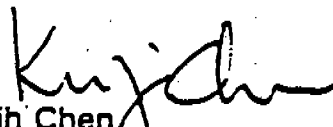
Twelve (12) Stainless Steel "SUMMA" Polished Canisters labeled:
"Inlet #1 (03/30/92)" "Inlet #2 (03/30/92)" "Inlet #3 (03/30/92)"
"Outlet #1 (03/30/92)" "Outlet #2 (03/30/92)" "Outlet #3 (03/30/92)"
"Inlet #1 (03/31/92)" "Inlet #2 (03/31/92)" "Inlet #3 (03/31/92)"
"Outlet #1 (03/31/92)" "Outlet #2 (03/31/92)" "Outlet #3 (03/31/92)"

The samples were received at the laboratory under chain of custody on April 2, 1992. The samples were received intact. The dates of analysis are indicated on the data sheets.

Twelve (12) six-liter passivated canisters were sent directly to the field sampler along with variable-constant differential low volume flow controllers. At the request of the sampler the flow controllers were calibrated to take one-hour time integrated samples. The majority of the canisters received by the laboratory were significantly undersampled. Ten of twelve canisters submitted to the laboratory were received under a unusually high vacuum. Canisters are evacuated to -14.0 psig at the laboratory prior to being sent out into the field. After time integrated sampling is completed, canisters returned to the laboratory generally have vacuum readings ranging from -2.5 psig to -0.5 psig. The ten canisters had vacuum readings of -12.5 psig to -8.9 psig, corresponding to sample volumes of 0.9 to 2.4 liters in a 6-liter container. In order to draw aliquots out of the canisters, the samples had to be pressurized with Nitrogen prior to laboratory analysis. The dilution factor due to the Nitrogen pressurization ranged from 3.22 to 8.50, thereby resulting in detection limits that are significantly higher than would otherwise be detected.

Data Release Authorization:

Reviewed and Approved:


Ju-jih Chen
Principal Chemist


Michael Tuday
Laboratory Director



Performance Analytical Inc.
Environmental Testing and Consulting

C1 through >C9 Hydrocarbon Analysis

The samples were analyzed for C₁ through >C₉ Hydrocarbons by direct injection GC/FID. The analytical system consisted of a Hewlett-Packard model 5890A gas chromatograph equipped with a flame ionization detector. Separation was achieved using a Restek RT₋₁ megabore column, 60 meters long by 0.53 mm I.D., with a 5.0 μ m film thickness.

A four point standard calibration was performed using a certified gas standard mix (Scott Speciality Gases) prior to analysis of the field samples.

Volatile Organic Compound Analysis

The samples were also analyzed by combined gas chromatography/mass spectrometry (GC/MS) for ten Volatile Organic Compounds. The analyses were performed according to the methodology outlined in EPA Method TO-14 from the Compendium of Methods for the Determination of Toxic Organic Compounds in Ambient Air, EPA 600/4-84-041, U.S. Environmental Protection Agency, Research Triangle Park, NC, April, 1984 and May, 1988. The analyses were performed by gas chromatography/mass spectrometry, utilizing a direct cryogenic trapping technique. The analytical system used was comprised of a Finnigan Model 4500C GC/MS/DS interfaced to a Tekmar 5010 Automatic Desorber. A thick film (5 micron) crossbonded 100% Dimethyl polysiloxane megabore column (RT₋₁, Restek Corporation, Bellefonte, PA) was used to achieve chromatographic separation.

The results of the analyses are included on the attached data sheets.



Performance Analytical Inc.
Environmental Testing and Consulting

PERFORMANCE ANALYTICAL INC.

RESULTS OF ANALYSIS

Client: San Diego Air Pollution Control District

Client Sample ID: N/A

PAI Sample ID: PAI Method Blank

Test Code: GC/MS EPA TO-14
Analyst: Chris Parnell
Instrument ID: Finnigan 4500C/Tekmar 5010
Verified by: Michael Tuday

Matrix: Summa Canister
Date Received: N/A
Date Analyzed: 04/08/92
Volume Analyzed: 1.00 Liter

CAS #	COMPOUND	RESULT (UG/M ³)	DETECTION LIMIT (UG/M ³)	RESULT (PPB)	DETECTION LIMIT (PPB)
75-01-4	VINYL CHLORIDE	ND	5.0	ND	2.0
75-09-2	METHYLENE CHLORIDE	ND	5.0	ND	1.5
67-66-3	CHLOROFORM	ND	5.0	ND	1.0
107-06-2	1,2-DICHLOROETHANE	ND	5.0	ND	1.2
71-55-6	1,1,1-TRICHLOROETHANE	ND	5.0	ND	0.93
71-43-2	BENZENE	ND	5.0	ND	1.6
56-23-5	CARBON TETRACHLORIDE	ND	5.0	ND	0.80
79-01-6	TRICHLOROETHENE	ND	5.0	ND	0.94
106-93-4	1,2-DIBROMOETHANE	ND	5.0	ND	0.65
127-18-4	TETRACHLOROETHENE	ND	5.0	ND	0.75

ND = Not Detected TR = Trace Level - Below Indicated Detection Limit



Performance Analytical Inc.
Environmental Testing and Consulting

PERFORMANCE ANALYTICAL INC.

RESULTS OF ANALYSIS

Client: San Diego Air Pollution Control District

Client Sample ID: N/A

PAI Sample ID: PAI Method Blank

Test Code: GC/MS EPA TO-14
Analyst: Kathleen Aguilera
Instrument ID: Finnigan 4500C/Tekmar 5010
Verified by: Michael Tuday

Matrix: Summa Canister
Date Received: N/A
Date Analyzed: 04/07/92
Volume Analyzed: 1.00 Liter

CAS #	COMPOUND	RESULT (UG/M ³)	DETECTION LIMIT (UG/M ³)	RESULT (PPB)	DETECTION LIMIT (PPB)
75-01-4	VINYL CHLORIDE	ND	5.0	ND	2.0
75-09-2	METHYLENE CHLORIDE	ND	5.0	ND	1.5
67-66-3	CHLOROFORM	ND	5.0	ND	1.0
107-06-2	1,2-DICHLOROETHANE	ND	5.0	ND	1.2
71-55-6	1,1,1-TRICHLOROETHANE	ND	5.0	ND	0.93
71-43-2	BENZENE	ND	5.0	ND	1.6
56-23-5	CARBON TETRACHLORIDE	ND	5.0	ND	0.80
79-01-6	TRICHLOROETHENE	ND	5.0	ND	0.94
106-93-4	1,2-DIBROMOETHANE	ND	5.0	ND	0.65
127-18-4	TETRACHLOROETHENE	ND	5.0	ND	0.75

ND = Not Detected TR = Trace Level - Below Indicated Detection Limit



Performance Analytical Inc.
Environmental Testing and Consulting

PERFORMANCE ANALYTICAL INC.

RESULTS OF ANALYSIS

Client: San Diego Air Pollution Control District

Client Sample ID: Inlet #3 (03/30/92) (3:00)

PAI Sample ID: 9201465 (Laboratory Duplicate)

Test Code: EPA-18
Analyst: Ku-Jih Chen
Instrument ID: HP5890/FID #4
Verified by: Michael Taday

Matrix: Summa Canister
Date Received: 04/02/92
Date Analyzed: 04/10/92
Volume Analyzed: 0.050 ml
 $P_1 = -12.2$ $P_2 = +4.0$ $DF = 7.48$

COMPOUND	RESULT (PPM)	DETECTION LIMIT (PPM)
C1 as Methane	650000	180
C2 as Ethane	ND	180
C3 as n-Propane	ND	140
C4 as n-Butane	ND	110
C5 as Pentane	ND	70
C6 as n-Hexane	ND	70
C7 as n-Heptane	ND	70
C8 as n-Octane	ND	70
C9 as n-Nonane	ND	70
> C9 as n-Nonane	ND	70

ND = Not Detected TR = Trace Level - Below Indicated Detection Limit

Test Witness - Avg

SDAPCD RULES

TEST	LIMIT	MEASURED	PASS/FAIL
E 53b SPECIFIC CONT.	0.10 gr/dscf	0.005 gr/dscf	NON-EXCEEDANCE

TEST RESULTS SUMMARY:

ITEM	I	Cs(12%)	E
UNITS	%	gr/dscf	lbs/hr
VALUE	108	0.0049	0.09

ENGINEERING SUMMARY

Qstd	TYPE OF FUEL	LOAD	RATE
dscfm		Tons/Hr	Tons
3246			

TEST PARAMETERS:

PROCEDURES:

The procedures and equipment utilized in these tests are based on EPA NSPS guidelines and from the EPA CFR 40, Standards Method 5. The sampling utilized a front-end filter (fig. 1).

CALCULATIONS:

All calculations are based on the EPA CFR 40, Standards Method 5, July 1, 1991, Parts 53-60, Appendix A, Methods 1-5 inclusive.

PARTICULATE SAMPLING:

The test consisted of sampling at 16 traverse points, 4 from 4 sampling ports (fig.2) collected from 84 inches below the stack (fig.3). All field data, SCEC's as well as SDAPCD's, were transferred to the computer printout. All calculations were done by computer and the emissions were compared to SDAPCD rules.

ANALYSES:

Gas: A CEM analysis was performed by SCEC.

Particulate: All procedures follow EPA guidelines, except where noted in the SDAPCD QA manual.

EQUIPMENT:

All testing and analysis equipment was calibrated according to EPA guidelines and performed by SCEC.

OVERVIEW OF THE TEST:

RUN #1:

LAB: Eliminated from the average

PM: Eliminated from the average

RUN #2:

LAB: Eliminated from the average

PM: Pass, but eliminated from the average

RUN #3:

LAB: PASS

PM: PASS

Because of the disparity in numbers between the District and SCEC, it was decided to use the District's values. The District used the values from Run #3 only, because it produced the only reliable numbers. A complete critique of the performance of SCEC's testing procedures and calculations are on page 4 and a data summary of all 3 runs are on page 5.

FIELD DATA & DATA SUMMARY:

[illegible]

	V_m	ΔP	ΔH	t_s	t_{box}	t_i	t_1 (in)	t_2 (out)	v_s
Average:	33.180	0.027	1.106	1437	not done	68	69.19	68.56	17.419

METER BOX PARAMETERS: Box ID = <u>NUTECH</u> $\Delta H@$ = _____ Y = <u>0.9766</u>		NOZZLE & PROBE: D_n = <u>0.587</u> in A_n = <u>0.2706</u> in ² C_p = <u>0.840</u>		MISCELLANEOUS: Maximum vacuum = <u>5.0</u> in. Hg. Circular stack (Y/N) = <u>YES</u> Silica gel (Y/N) = <u>YES</u>	
VOLUME: Initial leak rate = <u>0.000</u> cfm Pass/Fail <u>PASS</u> Final leak rate = <u>0.000</u> cfm Pass/Fail <u>PASS</u> V_m = <u>33.180</u> ft ³		PRESSURES: P_{bar} = <u>29.85</u> in Hg P_g = <u>0.00</u> in H ₂ O $V_{pw} @ t_s$ = <u>29.9200</u> in Hg $V_{pw} @ t_i$ = <u>N/A</u> in Hg		LABORATORY DATA: $m_n(\text{front})$ = <u>0.004675</u> g CO_2 = <u>7.81</u> % $m_n(\text{back})$ = <u>0.001960</u> g O_2 = <u>11.70</u> % $m_n(\text{total})$ = <u>0.00664</u> g CO = <u>0.00</u> % V_{lc} = <u>65.10</u> ml N_2 = <u>80.49</u> %	
STACK PARAMETERS: D_s = <u>3.50</u> ft Length = <u>3.50</u> ft A_s = <u>12.25</u> ft ²		TIME: θ = <u>60.0</u> min n = <u>16</u> points s = <u>3.8</u> min/pt		TEMPERATURES: t_1 = <u>69.19</u> °F t_i = <u>68</u> °F t_2 = <u>68.56</u> °F t_{box} = <u>not done</u> °F t_m = <u>68.88</u> °F t_s = <u>1437</u> °F	

CALCULATIONS:

TEMPERATURES:

01)	$t_s = (\sum t_s(n))/\text{total } n's$	
02)	$T_s = t_s + 460$	1437 °F
03)	$t_m = (\sum [(t_1(n) + t_2(n))/2])/\text{total } n's = (t_1 + t_2)/2$	1897 °R
04)	$T_m = (t_1 + t_2)/2 + 460$	69 °F
05)	$t_a = (\sum t_a(n))/\text{total } n's$	529 °R
06)	T_{std}	68 °F
		528 °R

PRESSURES:

07)	$P_{bar} = [(P @ S.L.) + (\text{ft. above S.L.} \cdot (-0.1 \text{ in Hg}/100\text{ft}))]$	
08)	$P_g = \text{read from pressure sensing device}$	29.85 in Hg
09)	$P_s = P_{bar} + (P_g/13.6)$	0.00 in H2O
10)	ΔH	29.85 in Hg
11)	$P_m = P_{bar} + (\Delta H/13.6)$	1.106 in H2O
12)	P_{std}	29.93 in Hg
		29.92 in Hg

VOLUME:

13)	$V_m = V_m(\text{end}) - V_m(\text{begin})$	
14)	Y	33.180 ft ³
15)	$V_m' = V_m \cdot Y$	0.9765
16)	$V_{pw} @ T = \text{from appendix}$	32.404 ft ³
17)	$\text{corr } V_{wm} = [(V_m' \cdot V_{pw} @ T_{imp}/P_s) \cdot P_m \cdot T_{std}]/(T_m \cdot P_{std})$	N/A in Hg
18)	$V_{m \text{ std}} = [V_{pw} \cdot (T_{std}/T_m) \cdot (P_{m}/P_{std})] - \text{corr } V_{wm}$	0.0000 ft ³
19)	$V_{ic} = (\sum \text{Volume of impingers})$	32.962 ft ³
20)	ϕ	65.10 ml
22)	M_{H2O}	0.00201 lb/ml
23)	$V_w \text{ std} = [(V_{ic} \cdot \phi \cdot R \cdot T_{std})/(P_{std} \cdot M_{H2O})] - \text{corr } V_{wm}$	18.00 g/g-mo
		3.0727 ft ³

MOISTURE:

24)	$B_{ws}(1) = (V_w \text{ std})/(V_w \text{ std} + V_{m \text{ std}})100$	8.67 %
25)	$V_{pw} @ T_s = \text{from appendix}$	29.92 in Hg
26)	$B_{ws}(2) = [(V_{pw} @ T_s/P_s) \cdot 100]$	100.23 %
27)	$B_{ws} = \text{lower value of equation 24 or 26}$	8.67 %

MOLECULAR WEIGHT:

28)	%CO ₂	
29)	%CO ₂	11.70 %
30)	%N ₂ + inerts + %CO	7.81 %
31)	$M_d = [0.440(\%CO_2)] + [0.320(\%O_2)] + [0.280(\%N_2 + \text{inerts} + \%CO)]$	80.49 %
32)	$M_s = M_d / (1 - B_{ws}) + 18.0 / B_{ws}$	29.72 g/g-mole
		28.70 g/g-mole

FLOW:

33)	ΔP	
34)	C_p	0.0270 in H2O
35)	$v_s = 85.49 \cdot C_p \cdot [(T_s \cdot \Delta P / (P_s \cdot M_s))]^{.5}$	0.840
36)	$A_s = 3.14 \cdot [(D_s)^2 / 4]$	17.419 ft ² /sec
37)	$Q_s = (v_s) \cdot A_s \cdot 60$	12.250 ft ³ /s
38)	$Q_{std} = 17.64 \cdot Q_s \cdot (1 - B_{ws}) \cdot P_s / T_s$	12803 acfm
		3246 dscfm

EMISSIONS:

FRONT HALF

39)	$m_n (\text{front})$	
40)	$C_s (\text{front}) = 15.43 \cdot m_n (\text{front}) / V_{m \text{ std}}$	0.00468 g
41)	$C_s (12\% \text{ front}) = (12/\%CO_2) \cdot C_s (\text{front})$	0.00223 grains/dscf
42)	$E (\text{front}) = (0.00457) \cdot (Q_{std}) \cdot C_s (\text{front})$	0.003 grains/dscf
		0.06 lbs/hr

BACK HALF

43)	$m_n (\text{back})$	
44)	$C_s (\text{back}) = 15.43 \cdot m_n (\text{back}) / V_{m \text{ std}}$	0.00196 g
45)	$C_s (12\% \text{ back}) = (12/\%CO_2) \cdot C_s (\text{back})$	0.00093 grains/dscf
46)	$E (\text{back}) = (0.00457) \cdot (Q_{std}) \cdot C_s (\text{back})$	0.001 grains/dscf
		0.06 lbs/hr

TOTAL

47)	$m_n (\text{total}) = m_n (\text{front}) + m_n (\text{back})$	
48)	$C_s (\text{total}) = 15.43 \cdot m_n (\text{total}) / V_{m \text{ std}}$	0.00664 g
49)	$C_s (12\% \text{ total}) = (12/\%CO_2) \cdot C_s (\text{total})$	0.00316 grains/dscf
50)	$E (\text{total}) = (0.00457) \cdot (Q_{std}) \cdot C_s (\text{total})$	0.005 grains/dscf
		0.06 lbs/hr
51)	$E.A. = [(\%O_2 - .5(\%CO)) \cdot 100] / [0.264(\%N_2) - (\%O_2) - 0.5(\%CO)]$	122.52 %

ISOKINETICS:

52)	$D_n =$	
53)	$A_n = 3.14 \cdot [(D_n)^2 / 4]$	0.557 in ²
54)	$I = 0.0450 \cdot (T_s \cdot V_{m \text{ std}} / P_s) \cdot V_s \cdot A_n \cdot \phi \cdot (1 - B_{ws})$	0.2706 in ⁴
		108.34 % = 108 %

LABORATORY:

RUN #1:

- 1) SCEC used only 50 mls of acetone for the FRONT half rinses. The water blank is 0 ppm, so there was no SOLV. WGT. value.
- 2) SCEC did not wash out the BACK half with acetone, so the SOLV. WGT. contribution was zero.
- 3) For the BACK HALF totals, SCEC did not allow the beakers to reach a constant weight and they took an incorrect average weight. The District had to correct for these errors.
- 4) As a result of the preceding items, SCEC's TOTAL of the particulate collected differed from the District's.

ISOKINETICS:

- 1) SCEC broke the probe/nozzle halfway through the test. As a consequence of this, they couldn't do the following:
 - a. SCEC could not collect the SDAPCD minimum of 40 ft³.
 - b. SCEC could not do a front half recovery.
- 2) The District had to correct for illogical stack temp. measurements.

CONCLUSION:

This entire run was eliminated from the average, because the low amount of collected particulate would not be an accurate representative sample of the flare.

LABORATORY:

RUN #2:

- 1) For the FRONT HALF totals, SCEC did not allow the beakers to reach a constant weight and they took an incorrect average weight. The District had to correct for these errors.
- 2) SCEC used only 50 mls of acetone for the FRONT half rinses. The water blank is 0 ppm, so there was no SOLV. WGT. value.
- 3) SCEC did not allow the filter to come to a constant weight, so the District had to correct for this.
- 4) SCEC did not wash out the BACK half with acetone, so the SOLV. WGT. contribution was zero.
- 5) For the BACK HALF totals, SCEC took an incorrect average weight. The District had to correct for these errors.
- 6) As a result of the preceding items, SCEC's NET WGT of the particulate collected, differed from the District's.

ISOKINETICS:

- 1) SCEC did not collect the SDAPCD minimum amount of 40 ft³.
- 2) The District had to correct for illogical stack temp. measurements.

CONCLUSION:

SCEC's isokinetic sampling data are acceptable, but there are too many gross errors in the laboratory weight analysis, after the District made the proper data corrections, to be able to make a confident decision on the accuracy of the collected data. Consequently, it was decided to eliminate all data from run #2 from the average.

LABORATORY:

RUN #3:

- 1) SCEC used only 50 mls of acetone for the FRONT half rinses. The water blank is 0 ppm, so there was no SOLV. WGT. value.
- 2) SCEC did not wash out the BACK half with acetone, so the SOLV. WGT. contribution was zero.
- 3) For the FRONT HALF totals, SCEC did not allow the beakers to reach a constant weight and they took an incorrect average weight. The District had to correct for these errors.
- 4) For the BACK HALF totals, SCEC took an incorrect average weight. The District had to correct for these errors.
- 5) As a result of the preceding items, SCEC's NET WGT of the particulate collected differed from the District's.

ISOKINETICS:

- 1) SCEC did not collect the SDAPCD minimum amount of 40 ft³.
- 2) The District had to correct for illogical stack temp. measurements.

CONCLUSION:

The data from this run are acceptable, after the District has made the necessary corrections.

AVERAGE:

CONCLUSION:

The District will use their numbers generated from SCEC's raw data. The District will use the values from only Run #3, as the Overall test average values, because Runs #2 & #3 are unacceptable. It is called the APCD average on the page 5. SCEC's average on page 5 consists only of the average of Runs #2 & #3.

TEMPERATURES:		APCD RUN 1	SOEC RUN 1	APCD RUN 2	SOEC RUN 2	APCD RUN 3	SOEC RUN 3	APCD AVG	SOEC AVG
01)	$T_s = (\sum T_s(n))/\text{total } n's$	1443	1246	1433	1255	1437	1437	1437	1346
02)	$T_s = T_s + 460$	1903	1715	1893	1715	1897	1897	1897	1808
	$T_m = (\sum ((1(n) + 2k(n))/2))/\text{total } n's$	71	71	71	71	69	69	69	70
	$T_m = (t1 + t2)/2 + 460$	531	531	531	531	529	529	529	530
05)	$T_m = (\sum T_m(n))/\text{total } n's$	68	68	68	68	68	68	68	68
06)	T_{std}	528	528	528	528	528	528	528	528
PRESSURES:									
07)	$P_{bar} = (P @ S.L.) + (\text{ft. above S.L.} \times 0.1 \text{ in Hg}/100\text{ft})$	29.85	29.85	29.85	29.85	29.85	29.85	29.85	29.85
08)	$P_g = \text{read from pressure sensing device}$	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
09)	$P_s = P_{bar} + (P_g/13.6)$	29.85	29.85	29.85	29.85	29.85	29.85	29.85	29.85
10)	ΔH	0.885	0.885	1.117	1.117	1.106	1.105	1.106	1.111
11)	$P_m = P_{bar} + (\Delta H/13.6)$	29.92	29.92	29.93	29.93	29.93	29.93	29.93	29.93
12)	P_{std}	29.92	29.92	29.92	29.92	29.92	29.92	29.92	29.92
VOLUME:									
13)	$V_m = V_m(\text{end}) - V_m(\text{begin})$	31.727	31.727	35.282	35.280	33.180	33.180	33.180	34.730
14)	Y	0.9766	0.9766	0.9766	0.9766	0.9766	0.9766	0.9766	0.9766
15)	$V_m = V_m \times Y$	30.985	30.985	35.433	35.430	32.404	32.404	32.404	33.917
16)	$V_{pw} @ T_s = \text{from appendix}$	N/A	N/A	N/A	N/A	N/A	N/A	N/A	N/A
17)	$\text{corr } V_{wm} = ((V_m \times V_{pw} @ T_s / P_s) \times P_m \times T_{std}) / (T_m \times P_{std})$	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
18)	$V_{m \text{ std}} = ((V_m \times (T_{std}/T_m) \times (P_m/P_{std})) - \text{corr } V_{wm})$	30.794	30.790	35.262	35.250	32.362	32.362	32.362	33.506
19)	$V_{ic} = (\sum \text{Volume of impingers})$	62.50	62.50	80.80	80.80	65.10	65.10	65.10	72.95
20)	δ	0.00201	0.00201	0.00201	0.00201	0.00201	0.00201	0.00201	0.00201
21)	R	21.85	21.85	21.85	21.85	21.85	21.85	21.85	21.85
22)	M_{wH2O}	18.00	18.00	18.00	18.00	18.00	18.00	18.00	18.00
23)	$V_{w \text{ std}} = (((V_{ic} \times R \times T_{std}) / (P_{std} \times M_{wH2O})) - \text{corr } V_{wm})$	2.9500	not done	3.8138	not done	3.0727	not done	3.0727	not done
CALCULATIONS:									
MOISTURE:									
24)	$B_{ws}(1) = (V_{w \text{ std}}) / (V_{w \text{ std}} + V_{m \text{ std}}) \times 100$	8.74	8.72	9.76	9.74	8.67	8.65	8.67	8.20
25)	$V_{pw} @ T_s = \text{from appendix}$	29.92	N/A	29.92	29.92	29.92	29.92	29.92	29.92
26)	$B_{ws}(2) = ((V_{pw} @ T_s) / P_s) \times 100$	100.23	N/A	100.23	N/A	100.23	100.23	100.23	N/A
27)	$B_{ws} = \text{lower value of equation 24 or 26}$	8.74	8.72	9.76	9.74	8.67	8.65	8.67	8.20
MOLECULAR WEIGHT:									
28)	%O ₂	11.55	11.55	11.69	11.69	11.70	11.70	11.70	11.70
29)	%CO ₂	8.03	8.08	7.92	7.92	7.81	7.81	7.81	7.87
30)	%N ₂ + inerts + %CO	80.42	80.42	80.39	80.39	80.49	80.49	80.49	80.44
31)	$M_d = [0.440(\text{CO}_2)] + [0.320(\text{O}_2)] + [0.280(\text{N}_2 + \text{inerts} + \text{CO})]$	29.75	29.75	29.73	29.73	29.72	29.72	29.72	29.72
32)	$M_s = M_d \times (1 - B_{ws}) + 18.0 \times (B_{ws})$	28.72	28.73	28.59	28.59	28.70	28.71	28.70	28.65
FLOW:									
33)	ΔP	0.0192	0.019	0.0267	0.027	0.0266	0.027	0.0266	0.027
34)	C_p	0.840	0.840	0.840	0.840	0.840	0.840	0.840	0.840
35)	$vs = 85.49 \times C_p \times [(T_s \times \Delta P) / (P_s \times M_s)]^{1/5}$	14.809	14.856	17.475	16.690	17.419	17.520	17.419	17.105
36)	$As = 3.14 \times [(D_s)^2 / 4]$	12.250	12.250	12.250	12.250	12.250	12.250	12.250	12.250
37)	$Q_s = (vs) \times As \times 60$	10885	10915	12844	12287	12803	12877	12803	12572
38)	$Q_{std} = 17.64 \times Q_s \times (1 - B_{ws}) \times P_s / T_s$	2749	2727	3223	3402	3246	3257	3246	3335
EMISSIONS:									
FRONT HALF									
39)	$mn (\text{front})$	0.00000	0.00000	0.00322	0.00550	0.00468	0.00790	0.00468	0.00675
40)	$C_s (\text{front}) = 15.43 \times mn (\text{front}) / V_{m \text{ std}}$	0.00000	0.00000	0.00141	0.00250	0.00223	0.00378	0.00223	0.00313
41)	$C_s (12\% \text{ front}) = (12 / \% \text{CO}_2) \times C_s (\text{front})$	0.0000	0.0000	0.0021	0.0037	0.0034	0.0058	0.0034	0.0047
42)	$E (\text{front}) = (0.00857) \times (Q_{std}) \times C_s (\text{front})$	0.00	0.00	0.04	0.07	0.06	0.10	0.06	0.09
BACK HALF									
43)	$mn (\text{back})$	0.01716	0.00169	0.00000	0.00630	0.00196	0.00126	0.00196	0.00478
44)	$C_s (\text{back}) = 15.43 \times mn (\text{back}) / V_{m \text{ std}}$	0.00860	0.00045	0.00000	0.00354	0.00093	0.00060	0.00093	0.00212
45)	$C_s (12\% \text{ back}) = (12 / \% \text{CO}_2) \times C_s (\text{back})$	0.0128	0.00128	0.0000	0.0055	0.0014	0.0009	0.0014	0.0032
46)	$E (\text{back}) = (0.00857) \times (Q_{std}) \times C_s (\text{back})$	0.20	0.20	0.00	0.11	0.03	0.03	0.03	0.07
TOTAL									
47)	$mn (\text{total})$	0.01716	0.00169	0.00322	0.01383	0.00664	0.00916	0.00664	0.01155
48)	$C_s (\text{total}) = 15.43 \times mn (\text{total}) / V_{m \text{ std}}$	0.00860	0.00045	0.00141	0.00608	0.00316	0.00436	0.00316	0.00522
49)	$C_s (12\% \text{ total}) = (12 / \% \text{CO}_2) \times C_s (\text{total})$	0.0128	0.00128	0.0021	0.0092	0.0049	0.0070	0.0049	0.0081
50)	$E (\text{total}) = (0.00857) \times (Q_{std}) \times C_s (\text{total})$	0.20	0.20	0.04	0.18	0.09	0.12	0.09	0.15
#REF:									
51)	D_n	119.31	not done	122.63	not done	122.52	not done	122.52	not done
KINETICS:									
52)	$An = 3.14 \times [(D_n)^2 / 4]$	0.63	0.63	0.63	0.63	0.59	0.59	0.59	0.61
53)	$i = 0.9450 \times T_s \times V_{m \text{ std}} / P_s \times vs \times An \times (1 - B_{ws})$	0.3117	0.3117	0.3117	0.3117	0.2706	0.2706	0.2706	0.2912
54)		106	107	103	98	108	103	108	100

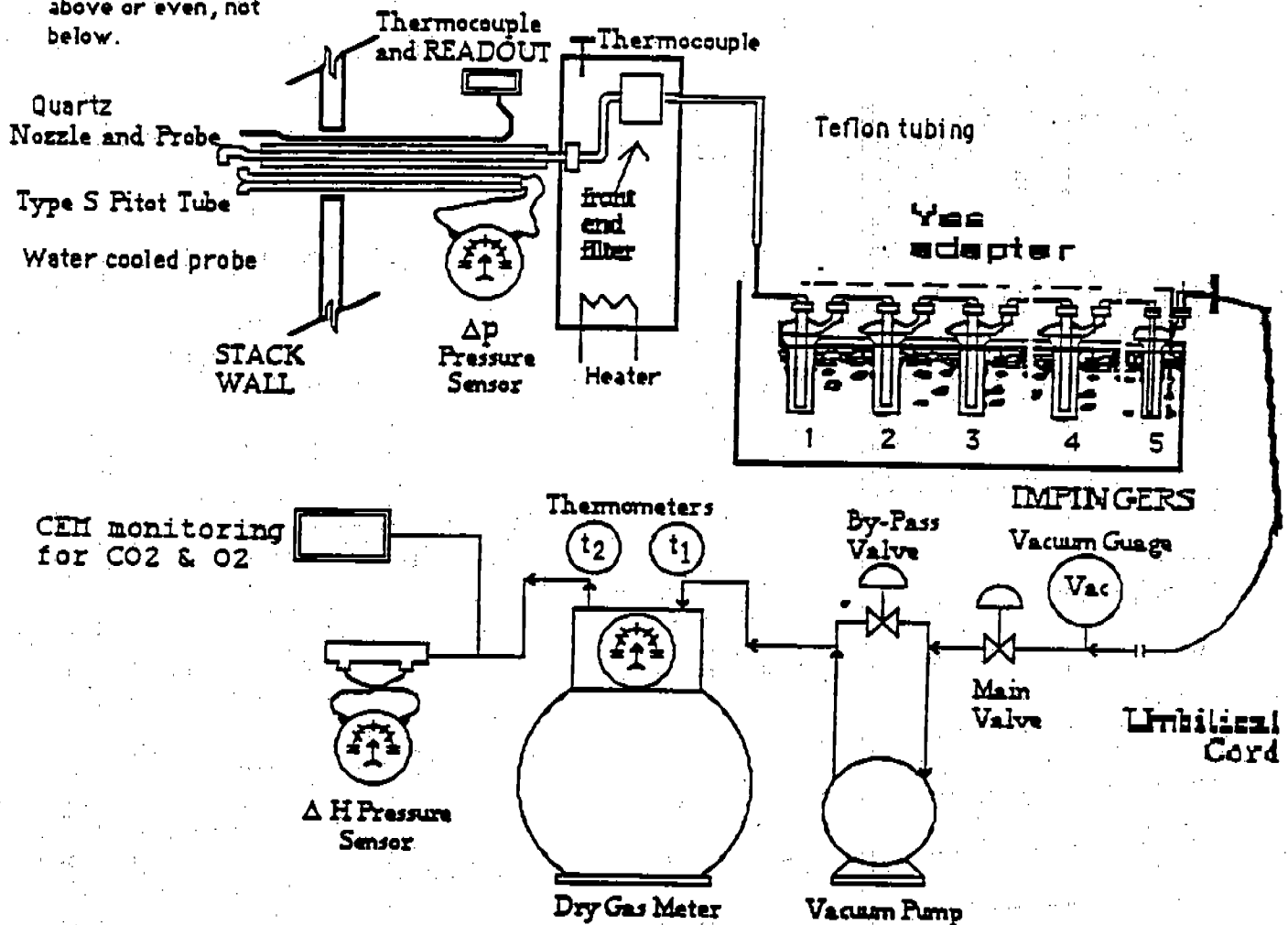
SAN DIEGO COUNTY AIR POLLUTION CONTROL DISTRICT

FIGURE 1

CONDENSOR SYSTEM

Note: 2.1.3

Pitot tube should be above or even, not below.



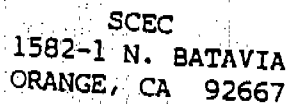
LEGEND

- No. 1 - IPa
- No. 2 - K.O.
- No. 3 - H2O2
- No. 4 - K.O.
- No. 5 - Silica Gel

FIELD DATA ABBREVIATIONS

- PT = Point Number
- Ts = Stack Temperature
- Δp = Pitot Tube Pressure Differential; in H₂O
- Vs = Stack Velocity, fps
- ΔH = Orifice Meter Pressure Drop, in H₂O
- t₁ = Meter Inlet Temperature, °F
- t₂ = Meter Outlet Temperature, °F
- Pm = Pump Vacuum, in Hg
- ti = Impinger Temperature
- P_{bar} = Barometric Pressure

FIGURE 1 : PARTICULATE MATTER SAMPLING TRAIN



SAMPLE POINT LOCATION DATA SHEET

H= _____

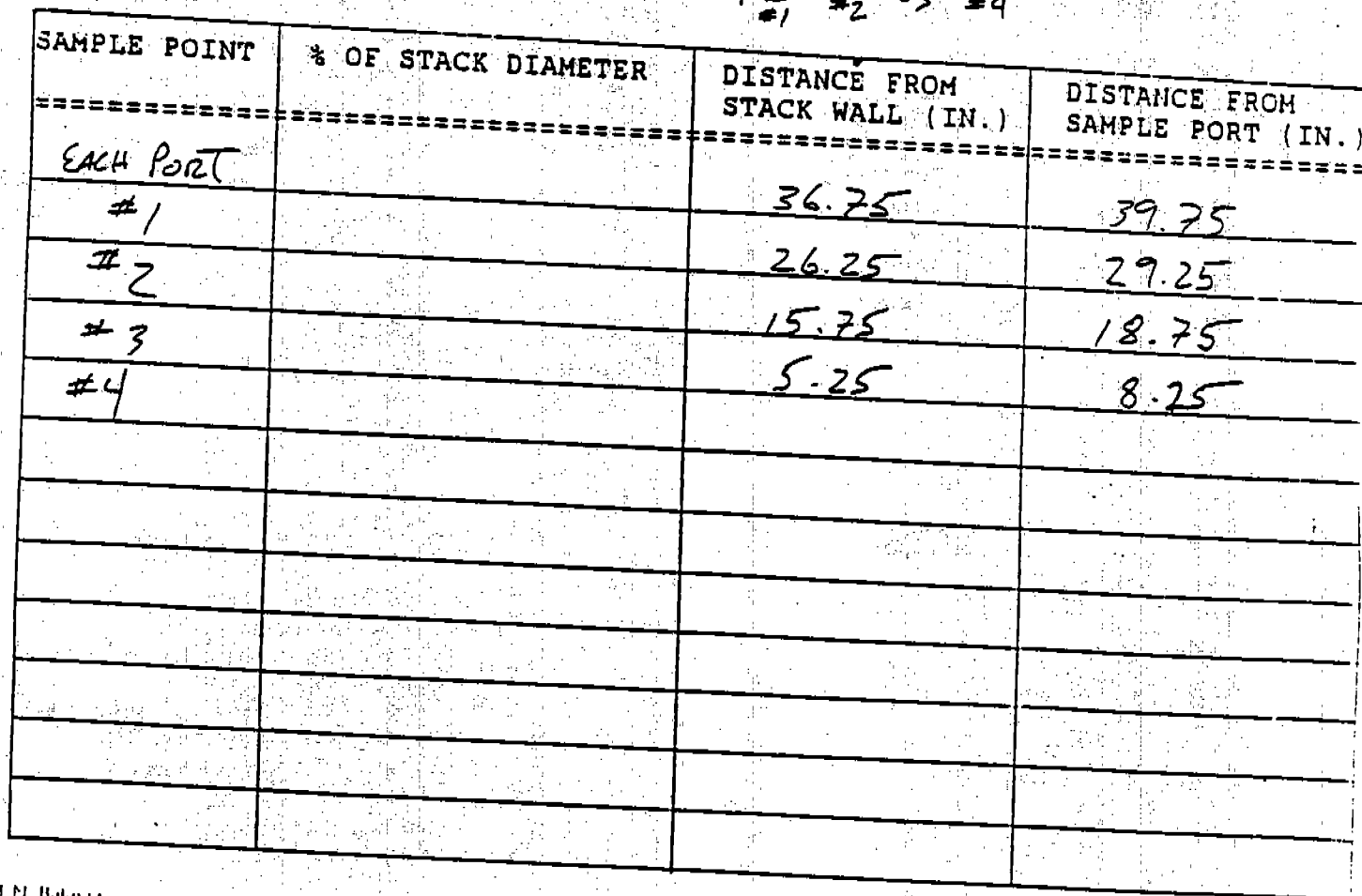
UPSTREAM DIST./
EQUIVALENT DIAMETERS 5

DOWNSTREAM DIST./
EQUIVALENT DIAMETERS 2

NO. OF SAMPLING POINTS _____

SAMPLING PORT DIMENSIONS:
DIA. = 3"

PROTRUSION DIST. = 3"



Figure

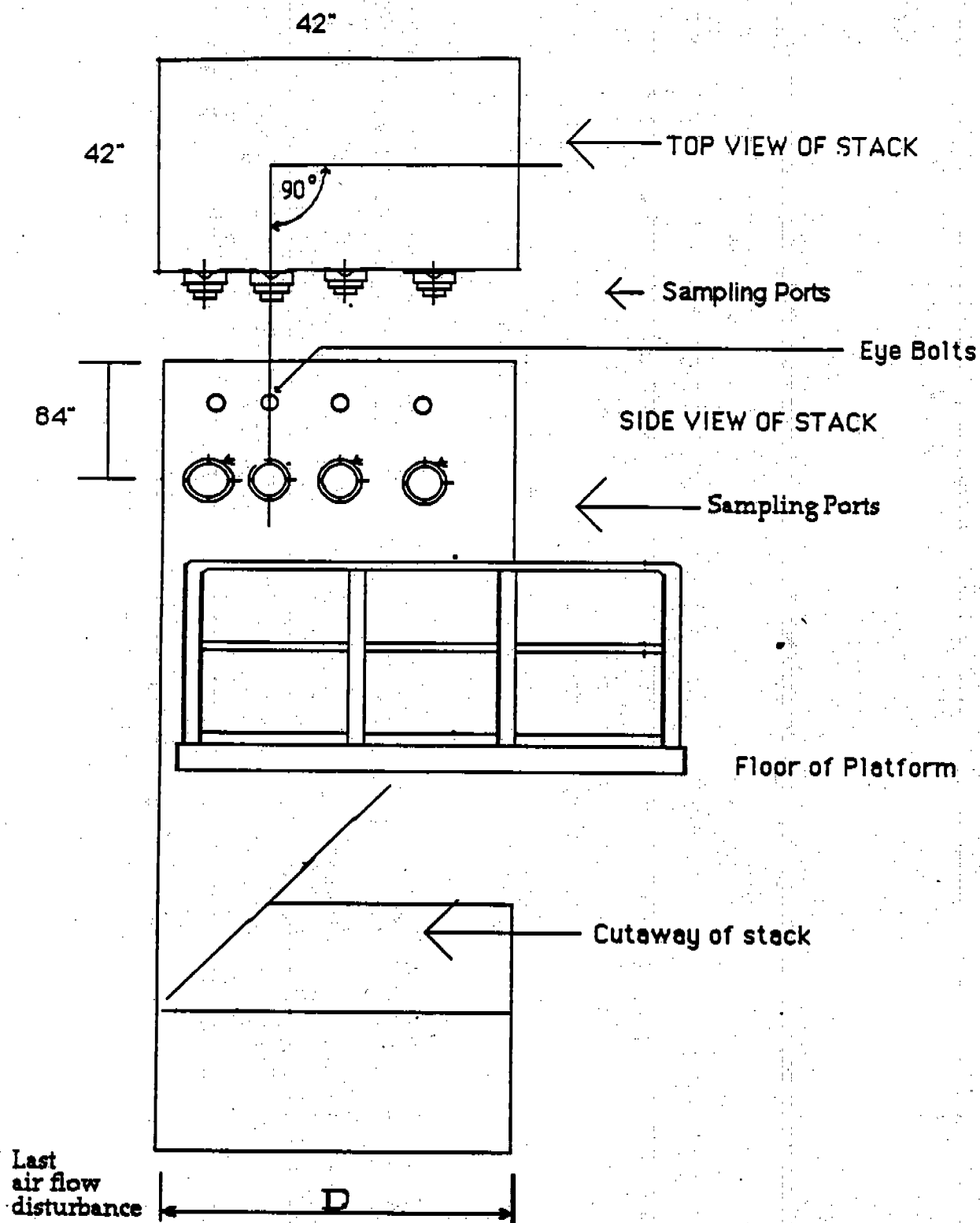


Figure 3

NOMENCLATURE

symbol	units	explanation	equation
A			
An	in ²	nozzle area	$\pi/4(D_n)^2$
As	ft ²	stack area	$\pi/4(D_s)^2$ or $L \times W$
B			
Bws(1)	%	fractional stack gas moisture-equ 1	$((V_w \text{ std})/(V_w \text{ std} + V_m \text{ std}))100$
Bws(2)	%	fractional stack gas moisture-equ 2	$((V_{pw} @ ts)/P_s)100$
Bws	%	water vapor in the gas stream	lower of Bws(1) and Bws(2)
C			
CO	%	carbon monoxide	read from measuring device (0 for Asphalt plants)
CO2	%	carbon dioxide	read from measuring device
Corr Vwm	ft ³	correction for Vw w/o silica gel	$((V_m \times (V_{pw} @ ts)/P_s) \times P_m \times T_{std}) / (T_m \times P_{std})$
Cp	none	pitot tube correction factor	see EPA method 3
Cs(front)	gr/dscf	concentration of particulate in stack gas, corrected to STP-for front	$(15.43 \times mn(\text{front})) / (V_m \text{ std})$
Cs(back)	gr/dscf	concentration of particulate in stack gas, corrected to STP-for back	$(15.43 \times mn(\text{back})) / (V_m \text{ std})$
Cs(total)	gr/dscf	concentration of particulate in stack gas, corrected to STP-for total	$(15.43 \times mn(\text{total})) / (V_m \text{ std})$
Cs12(front, back, total)		same as Cs(front, back, total) except-corrected for grain loading at 12% CO2	$((12/\%CO_2) \times (15.43 \times mn(\text{fr, back, total}))) / (V_m \text{ std})$
D			
∂ (density)	lb/ml	density of water at STP	0.002201 (see CRC)
Ds	in or ft	stack diameter	measure at site
Dn	in	nozzle diameter	avg of at least three measurements
E			
EA	%	Excess air (for combustion)	$((\%CO_2 - 5\%CO) \times 100) / (26.4 \times \%N_2 - \%CO_2 - 5\%CO)$
E(front)	lbs/hr	part. emissions rate-front	$(0.00857)(Q_s \times C_s(\text{front}))$
E(back)	lbs/hr	part. emissions rate-back	$(0.00857)(Q_s \times C_s(\text{back}))$
E(total)	lbs/hr	part. emissions rate-total	$(0.00857)(Q_s \times C_s(\text{total}))$
H			
ΔH	in H2O	average differential pressure across the orifice meter	avg of the readings from the pressure measuring device
ΔH@	none	orifice pressure differential at STP	see EPA Method 5 Appendix
I			
I	%	isokinetics	$(0.09450 \times T_s \times V_m \text{ std}) / [P_s \times r^2 \times (A_n / 144) \times (1 - (Bws/100))]$
M			
Md	g/g-mole	dry stack gas molecular wgt	$0.44(\%CO_2) + 0.320(\%O_2) + 0.280(\%N_2 + \text{inerts} + CO)$
mn(back)	g	particulate in impingers	measurement from lab analysis
mn(front)	g	particulate in nozzle & probe	measurement from lab analysis
mn(total)	g	total particulate collected	measurement from lab analysis
Ms	g/g-mole	wet stack gas molecular wgt	$Md(1 - Bws) + 18.0(Bws)$
MW CO2	g/mole	mo. wgt of carbon dioxide	44 (see periodic table)
MW N2	g/mole	mo. wgt of nitrogen	28 (see periodic table)
MW O2	g/mole	mo. wgt of oxygen	32 (see periodic table)
MW H2O	g/mole	mo. wgt of water	18 (see periodic table)
N			
N2	%	percent nitrogen	$100 - (\%CO_2 + \%O_2 + \%CO + \text{inerts})$
O			
O2	%	percent oxygen	read from measuring device

NOMENCLATURE (cont.)

OMENCLATURE (concl.)

symbol	units	explanation	equation
P			
ΔP	in H ₂ O	pilot diff. press-velocity head of stack gas	read from measuring device
P_s	in Hg	barometric pressure at sampling pt.	read from press measuring device
$\pi(p)$	none	the ratio of the circumference of a circle to its diameter	3.14165 (see CRC)
P_m	in Hg	absolute meter pressure	$P_{bar} + (\Delta H/13.6)$
P_s	in Hg	absolute stack pressure	$P_{bar} + (P_{static}/13.6)$
P_g	in H ₂ O	static pressure of stack	read from pressure sensing device
P_{std}	in Hg	press at std conditions (29.92)	see CFR
Q			
Q_s	acfm	flow rate	$vs \cdot A_o \cdot 60$
Q_{std}	dscfm	dry volumetric stack gas flow rate, corrected to STP	$17.64 \cdot Q_s (1 - B_{ws}) \cdot (P_s/T_s)$
R			
R	in Hg-ft ³ /°R-lb-mo	ideal gas constant	21.85 (see CRC)
S			
S.L.	none	Sea Level	read from a relief map
T			
t_1	°F	dry gas meter inlet temp, uncorrected	read from temp sensing device
t_2	°F	dry gas meter outlet temp, uncorrected	read from temp sensing device
$t_1 \text{ corr}$	°F	dry gas meter outlet temp, corrected	$t_1 + \text{temperature correction}$
$t_2 \text{ corr}$	°F	dry gas meter outlet temp, corrected	$t_2 + \text{temperature correction}$
$a(\theta)$	min	sampling time/point	Q/t_n
$\theta(\theta)$	min	total sampling time	none
t_i	°F	impinger outlet temp	read from temp sensing device
t_m	°F	dry gas meter temp in F	$(t_1 + t_2)/2$
T_m	°R	dry gas meter temp in R	$t_m + 460$
t_n	none	t_i number or traverse pts	summation of the traverse points
t_s	°F	stack temp in F	read from temp sensing device
T_{std}	°R	stack temp in R	$t_s + 460$
t_{std}	°R	temp at std conditions (528)	see CFR
U			
V_{lc}	ml	water collected from impingers and the silica gel (if applicable)	from lab analysis
V_m	ft ³	sample gas volume, uncorrected	read from dry gas meter
V_m'	ft ³	sample gas volume, corrected	$V_m \cdot Y$
$V_m \text{ std}$	ft ³	volume of gas sample by the dry gas meter, corrected to STP	$((V_m \cdot T_{std})/P_m)/((P_{std} \cdot T_m) - \text{corr } V_m)$
$V_{pw@ts}$	in Hg	vapor pressure of water at t_s	see CRC water vapor press. tables
$V_{pw@ti}$	in Hg	vapor pressure of water at t_i	see CRC water vapor press. tables
V_s	ft/sec	stack gas velocity	$85.49 \cdot C_p \cdot ((T_s \cdot \Delta P)/(P_s \cdot M_s))^{0.5}$
$V_w \text{ std}$	ft ³	Vol. of water vapor in gas sample, corrected to STP	$(V_{lc} \cdot R \cdot T_{std})/(P_{std} \cdot MW_{H_2O}) + \text{corr } V_{wm}$
Y			
Y	none	dry gas meter calibration factor	see CFR 40, parts 53-60

Conversion Factors

(multiply by the number)

0.002669	in Hg-ft ³ /°R-ml	conversion to get in Hg-ft ³ /R	see CRC
0.00857	lb/gr-min/hr	conv from gr/min to lb/hr (60/7000)	see Lange's Handbook of Chemistry
0.04707	ft ³ /ml	conversion from ml to ft ³	see Lange's Handbook of Chemistry
15.43	gr/g	conversion from g to gr	see Lange's Handbook of Chemistry
17.64	°R/in H ₂ O	T_{std}/P_{std} (528/29.92)	see Lange's Handbook of Chemistry
85.49	$(\text{ft/sec}) \cdot (\text{lb-in Hg/lb-mo} \cdot \text{°R-in H}_2\text{O}))^{0.5}$	conversion factor to get velocity in ft/sec	see CRC

(divide by the number)

144	in ² /ft ²	conversion from in ² to ft ²	see CRC
13.6	in H ₂ O/in Hg	conversion from in H ₂ O to in Hg	see CRC

(add to the number)

...	°R/°F	conversion from F to R	see CRC
-----	-------	------------------------	---------

SAN DIEGO AIR POLLUTION CONTROL DISTRICT
MONITORING AND TECHNICAL SERVICES
9150 CHESAPEAKE DRIVE
SAN DIEGO, CA 92123

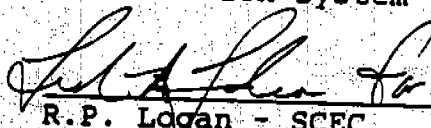
NITROGEN OXIDES, CARBON MONOXIDE, PARTICULATE,
AND SULFUR EMISSIONS SUMMARY REPORT

SITE: Arizona Street Flare

P/O NUMBER: 56896 and 59383 JOB NO: T1482-1

TEST DATE: 3/30/92

EQUIPMENT: Arizona Street Landfill Gas Collection and Incineration System

REPORT BY:  DATE: 5/14/92
R.P. Logan - SCEC

APCD PERSONNEL: Janet Cawyer/David Shina

SITE PERSONNEL: Ray Purtee

APPROVED BY: _____ DATE: _____

SCEC
1582-1 N. BATAVIA
ORANGE, CA 92667
(714)282-8240

COMPANY: S.D.A.P.C.D. @ ARIZONA STREET
DATE: MARCH 30, 1992
UNIT: FLARE @ EXHAUST
REPORT #: T1482-1

FIELD DATA @ 68'

SITE:

	RUN #:	1	2	3
	TIME:	1125	1403	1600
Vm (dry gas sampled).....	31.727	36.28	33.18	
Y (meter calib. factor).....	0.976583	0.976583	0.976583	
P bar (Barometric pressure).....	29.85	29.85	29.85	
P static (stack pressure, " H2O).....	0	0	0	
Delta H (differential meter press, " H2O)....	0.885	1.117	1.105	
Tm (meter temperature, R').....	531.2	530.93	528.88	
Vol H2O mls	62.5	80.8	65.1	
Vm(std),dscf	30.79	35.25	32.36	
Bws-H2O vapor	0.0872	0.0974	0.0865	
MF-moisture factor	0.9128	0.9026	0.9135	
% CO2	8.03	7.92	7.81	
% O2	11.55	11.69	11.7	
% N2	80.42	80.39	80.49	
Md-MW stk gas,dry	29.75	29.73	29.72	
Ms-MW stk gas,wet	28.73	28.59	28.71	
Cp-pitot tube	0.84	0.84	0.84	
Avg sq rt ^p	0.138	0.164	0.164	
T stack, R'.....	1924.77	1714.5	1896.7	
Stack area,ft2	12.25	12.25	12.25	
Vs-fps	14.85	16.69	17.52	
Qstd-dscfm	2727	3402	3267	
Area noz,ft2	2.16E-03	2.16E-03	1.88E-03	
Sample time	60	60	60	
% Isokinetic	106.5	97.7	107.6	

SOURCE TEST OF PARTICULATE EMISSIONS TO THE ATMOSPHERE

TEST SITE: Balboa Park Landfill Flare
 2850 Pershing Dr.
 San Diego, CA

TEST WITNESS - RUN #1

TEST #: 92090.1

P.O.#: none

TEST DATE: 3/30/92

Type of plant (Asphalt/Perlite/Combustion):

COMBUSTION

UNIT TESTED: INCINERATOR

EQUIPMENT: LANDFILL FLARE

TESTED BY: Russ Logan & Ted Jackman of SCEC

DATE: 3/30/92

SITE PERSONNEL: Ray Purtee

DATE: 3/30/92

APCD ENGINEER: Archi de la Cruz

DATE: 3/30/92

LAB ANALYSIS BY: SCEC

DATE: 4/21/92

REPORT BY: SCEC (Russ Logan)

DATE: 5/14/92

REVIEWED BY: David N. Shina

DATE: 6/29/92

APPROVED BY:

DATE:

JUDITH LAKE, CHIEF OF MONITORING

This report has been reviewed and found to be representative of the testing that was performed.

SDAPCD RULES

TEST	LIMIT	MEASURED	PASS/FAIL
RULE 53 SPECIFIC CONT.	0.10 gr/dscf	0.013 gr/dscf	NON-EXCEEDANCE

TEST RESULTS SUMMARY:

ITEM	I	Cs(12%)	E
UNITS	%	gr/dscf	lbs/hr
VALUE	106	0.0128	0.20

ENGINEERING SUMMARY

Qstd	TYPE OF FUEL	LOAD	RATE
dscfm		Tons/Hr	Tons
2749			

TEST PARAMETERS:

SYSTEM DESCRIPTION:

Landfill gas is sucked through the piping of this system. The landfill gas is constantly being burned off by the flare combustion system. The flare is at the bottom of the incinerator stack. The sampling points are near the top of the stack. The particulate emissions from this process are the subject of the report.

PROCEDURES:

The procedures and equipment utilized in these tests are based on EPA New Source Performance Standards Method 5. The sampling train utilized a front-end filter (fig. 1)

CALCULATIONS:

All equations are from EPA CFR 40, July 1, 1991, Parts 53-60, Appendix A, Methods 1-5 inclusive.

PARTICULATE SAMPLING:

The test consisted of sampling at 16 traverse points, 4 from each of 4 sample ports (fig.2), collected from 84 inches below the stack (fig.3). All field data was transferred to the computer printout. All calculations were done by the computer and the emissions were compared to rule 53b of the SDAPCD.

ANALYSES:

Gas: A CEM analysis was performed by SCEC.

Particulates: All procedures follow EPA guidelines, except where noted in the SDAPCD QA manual.

EQUIPMENT:

All testing and analysis equipment was calibrated according to EPA guidelines and done by SCEC.

FIELD DATA & DATA SUMMARY:

Trav. Pt	Vm (ft ³)	ΔP (in H ₂ O)	ΔH (in H ₂ O)	Stack Temp (°F)	Box Temp (°F)	Imp Temp (°F)	t 1 (in) (°F)	t 2 (out) (°F)	velocity (ft/sec)
	297.665								
A1		0.010	1.500	1400		68	71	70	018.58
2		0.020	0.680	1420		68	71	70	015.04
3		0.030	0.700	1468		68	73	71	015.23
4		0.010	0.340	1420		68	73	71	010.63
B1		0.010	0.750	1470		68	73	72	010.77
2		0.010	0.700	1440		68	73	71	010.69
3		0.030	0.660	1478		68	73	71	015.27
4		0.020	0.670	1468		68	73	71	015.23
C1		0.020	1.340	1460		68	71	71	015.20
2		0.030	1.030	1460		68	72	70	018.61
3		0.030	1.000	1461		68	71	71	018.62
4		0.030	1.000	1457		68	71	70	018.60
D1		0.010	0.740	1470		68	72	69	010.77
2		0.020	0.710	1340		68	71	70	014.72
3		0.030	1.000	1472		68	71	70	018.67
4	329.392	0.030	1.040	1398		68	71	70	018.31
Average:									
	Vm	ΔP	ΔH	***ts	tbox	tl	t 1 (in)	t 2 (out)	vs
	31.727	0.019	0.885	1443	not done	68	71.88	70.50	14.81

*** SSEC took their thermocouple readings of the first point of each port too early (when they changed ports, the thermocouple cooled down to c.a. 300-500 °F). I had to correct the temperatures at the beginning of each port change. Their temperatures were too low. To correct for this, I gave the first point of each port the average of the previous three temperatures.

METER BOX PARAMETERS: Box ID = <u>NUTECH</u> $\Delta H@$ = _____ Y = <u>0.9766</u>	NOZZLE & PROBE: Dn = <u>0.630</u> in An = <u>0.3117</u> in ² Cp = <u>0.840</u>	MISCELLANEOUS: Maximum vacuum = <u>5.0</u> in. Hg. Circular stack (Y/N) = <u>YES</u> Silica gel (Y/N) = <u>YES</u>
VOLUME: start leak rate = <u>0.000</u> cfm Pass/Fail <u>PASS</u> final leak rate = <u>0.000</u> cfm Pass/Fail <u>PASS</u> Vm <u>31.727</u> ft ³	PRESSURES: Pbar = <u>29.85</u> in Hg Pg = <u>0.00</u> in H ₂ O Vpw @ ts = <u>29.9200</u> in Hg Vpw @ ti = <u>N/A</u> in Hg	LABORATORY DATA: mn(front) = <u>0.00000</u> g CO ₂ = <u>8.03</u> % mn(back) = <u>0.01716</u> g O ₂ = <u>11.55</u> % mn(total) = <u>0.01716</u> g CO = <u>0.00</u> % Vlc <u>62.50</u> ml N ₂ = <u>80.42</u> %
STACK PARAMETERS: Ds = <u>3.50</u> ft Length = <u>3.50</u> ft As = <u>12.25</u> ft ²	TIME: ϕ = <u>60.0</u> min tn = <u>16</u> points s = <u>3.8</u> min/pt	TEMPERATURES: t1 = <u>71.88</u> °F ti = <u>68</u> °F t2 = <u>70.50</u> °F tbox = <u>not done</u> °F tm = <u>71.19</u> °F ts = <u>1443</u> °F

CALCULATIONS:**TEMPERATURES:**

01)	$t_s = (\sum t_s(n))/\text{total } n's$	
02)	$T_s = t_s + 460$	1443 °F
03)	$t_m = (\sum ((t_1(n) + t_2(n))/2))/\text{total } n's = (t_1 + t_2)/2$	1903 °R
04)	$T_m = (t_1 + t_2)/2 + 460$	71 °F
05)	$t_i = (\sum t_i(n))/\text{total } n's$	531 °R
06)	T_{std}	68 °F 528 °R

PRESSURES:

07)	$P_{bar} = ((P @ S.L.) + [\text{ft. above S.L.} \cdot (-0.1 \text{ in Hg}/100\text{ft})])$	
08)	$P_g = \text{read from pressure sensing device}$	29.85 in Hg
09)	$P_s = P_{bar} + (P_g/13.6)$	0.00 in H ₂ O
10)	ΔH	29.85 in Hg
11)	$P_m = P_{bar} + (\Delta H/13.6)$	0.885 in H ₂ O
12)	P_{std}	29.92 in Hg 29.92 in Hg

VOLUME:

13)	$V_m = V_m(\text{end}) - V_m(\text{begin})$	
14)	Y	31.727 ft ³
15)	$V_m' = V_m \cdot Y$	0.9766
16)	$V_{pw} @ t_i = \text{from appendix}$	30.985 ft ³
17)	$\text{corr } V_{wm} = (((V_m' \cdot V_{pw} @ \text{imp}/P_s) \cdot P_m \cdot T_{std}) / (T_m \cdot P_{std}))$	N/A in Hg
18)	$V_m \text{ std} = [V_m' \cdot (T_{std}/T_m) \cdot (P_m/P_{std})] - \text{corr } V_{wm}$	0.0000 ft ³
19)	$V_{ic} = (\sum \text{Volume of Impingers})$	30.794 ft ³
20)	Z	62.50 ml
21)	R	0.002010 lb/ml
22)	M_{wH_2O}	21.85 in Hg-ft ³ /°R-lb-mo
23)	$V_w \text{ std} = (((V_{ic} \cdot Z \cdot R \cdot T_{std}) / (P_{std} \cdot M_{wH_2O})) + \text{corr } V_{wm})$	18.88 g/g-mo 2.9500 ft ³

MOISTURE:

24)	$B_{ws}(1) = (V_w \text{ std} / (V_w \text{ std} + V_m \text{ std})) \cdot 100$	8.74 %
25)	$V_{pw} @ t_s = \text{from appendix}$	29.92 in Hg
26)	$B_{ws}(2) = ((V_{pw} @ t_s / P_s) \cdot 100)$	100.23 %
27)	$B_{ws} = \text{lower value of equation 24 or 26}$	8.74 %

MOLECULAR WEIGHT:

28)	%O ₂	
29)	%CO ₂	11.55 %
30)	%N ₂ +inerts+%CO	8.03 %
31)	$M_d = [0.440(\%CO_2)] + [0.320(\%O_2)] + [0.280(\%N_2 + \text{inerts} + \%CO)]$	80.42 %
32)	$M_s = M_d \cdot (1 - B_{ws}) + 18.0 \cdot B_{ws}$	29.75 g/g-mole 28.72 g/g-mole

FLOW:

33)	ΔP	
34)	C_p	0.0192 in H ₂ O
35)	$v_s = 85.49 \cdot C_p \cdot [((T_s \cdot \Delta P) / (P_s \cdot M_s))]^{0.5}$	0.840
36)	$A_s = 3.14 \cdot [(D_s)^2 / 4]$	14.809 ft ² /sec
37)	$Q_s = (v_s) \cdot A_s \cdot 60$	12.250 ft ³ /s
38)	$Q_{std} = 17.64 \cdot Q_s \cdot (P_{std} / P_s) \cdot (T_s / T_{std})$	10885 acfm 2740 dscfm

EMISSIONS:**FRONT HALF**

39)	$m_n (\text{front})$	
40)	$C_s (\text{front}) = (12\% \cdot CO_2) \cdot C_s (\text{total})$	0.00000 g
41)	$C_s (12\%, \text{front}) = (12\% \cdot CO_2) \cdot C_s (\text{front})$	0.00000 grains/dscf
42)	$E (\text{front}) = (Q_{std} / 35.3147) \cdot C_s (12\%, \text{front})$	0.000 grains/dscf 0.00 lb/hr

BACK HALF

43)	$m_n (\text{back})$	
44)	$C_s (\text{back}) = (12\% \cdot CO_2) \cdot C_s (\text{total})$	0.01716 g
45)	$C_s (12\%, \text{back}) = (12\% \cdot CO_2) \cdot C_s (\text{back})$	0.00650 grains/dscf
46)	$E (\text{back}) = (Q_{std} / 35.3147) \cdot C_s (12\%, \text{back})$	0.013 grains/dscf 0.20 lb/hr

TOTAL

47)	$m_n (\text{total}) = m_n (\text{front}) + m_n (\text{back})$	
48)	$C_s (\text{total}) = 12\% \cdot CO_2 \cdot C_s (\text{total})$	0.01716 g
49)	$C_s (12\%, \text{total}) = (12\% \cdot CO_2) \cdot C_s (\text{total})$	0.00650 grains/dscf
50)	$E (\text{total}) = (Q_{std} / 35.3147) \cdot C_s (12\%, \text{total})$	0.013 grains/dscf 0.20 lb/hr
51)	$E.A. = ((\%O_2 - 0.5(\%CO)) \cdot 100) / [0.264(\%N_2) - (\%O_2) - 0.5(\%CO)]$	119.31 %

ISOKINETICS:

52)	D_n	
53)	$A_n = 3.14 \cdot [(D_n)^2 / 4]$	0.830 in ²
54)	$L = 0.450 \cdot (T_s \cdot V_m \text{ std} / P_s \cdot V_s \cdot A_n \cdot (1 - B_{ws}))$	0.3117 in ² 105.67 % = 105 %

SOURCE TEST OF PARTICULATE EMISSIONS TO THE ATMOSPHERE

TEST SITE: Balboa Park Landfill Flare
 2850 Pershing Dr.
 San Diego, CA

TEST #: 92090.2

P.O.#: none

TEST DATE: 3/30/92

Type of plant (Asphalt/Perlite/Combustion):

COMBUSTION

UNIT TESTED: INCINERATOR

TEST WITNESS - RUN #2

EQUIPMENT: LANDFILL FLARE

TESTED BY: Russ Logan & Ted Jackman of SCEC

DATE: 3/30/92

SITE PERSONNEL: Ray Purtee

DATE: 3/30/92

APCD ENGINEER: Archi de la Cruz

DATE: 3/30/92

LAB ANALYSIS BY: SCEC

DATE: 4/21/92

REPORT BY: SCEC (Russ Logan)

DATE: 5/14/92

REVIEWED BY: David N. Shina

DATE: 6/29/92

APPROVED BY:

DATE:

JUDITH LAKE, CHIEF OF MONITORING

This report has been reviewed and found to be representative of the testing that was performed.

SDAPCD RULES

TEST	LIMIT	MEASURED	PASS/FAIL
E 53 SPECIFIC CONT.	0.10 gr/dscf	0.0021 gr/dscf	NON-EXCEEDANCE

TEST RESULTS SUMMARY:

ITEM	I	Cs(12%)	E
UNITS	%	gr/dscf	lbs/hr
VALUE	103	0.0021	0.04

ENGINEERING SUMMARY

Qstd	TYPE OF FUEL	LOAD	RATE
dscfm		Tons/Hr	Tons
3223			

TEST PARAMETERS:

SYSTEM DESCRIPTION:

Landfill gas is sucked through the piping of this system. The landfill gas is constantly being burned off by the flare combustion system. The flare is at the bottom of the incinerator stack. The sampling points are near the top of the stack. The particulate emissions from this process are the subject of the report.

PROCEDURES:

The procedures and equipment utilized in these tests are based on EPA New Source Performance Standards Method 5. The sampling train utilized a front-end filter (fig. 1)

CALCULATIONS

All equations are from EPA CRR 40, July 1, 1991, Parts 53-60, Appendix A, Methods 1-5 inclusive.

PARTICULATE SAMPLING

The test consisted of sampling at 16 traverse points, 4 from each of 4 sample ports (fig.2), collected from 84 inches below the stack (fig.3). All field data was transferred to the computer printout. All calculations were done by the computer and the emissions were compared to rule 53b of the SDAPCD.

ANALYSES:

Gas: A CEM analysis was performed by SCEC.

Particulate: All procedures follow EPA guidelines, except where noted in the SDAPCD QA manual.

EQUIPMENT:

All testing and analysis equipment was calibrated according to EPA guidelines and done by SCEC.

FIELD DATA & DATA SUMMARY:

P.O.#none TEST #92090.2

Trav. Pt	Vm (ft ³)	ΔP (in H ₂ O)	ΔH (in H ₂ O)	Stack Temp (°F)	Box Temp (°F)	Imp Temp (°F)	t 1 (in) (°F)	t 2 (out) (°F)	velocity (ft/sec)
	330.003								
A1		0.020	1.440	1450		68	71	70	015.19
2		0.030	1.000	1460		68	73	71	018.66
3		0.030	1.010	1452		68	72	70	016.62
4		0.030	1.020	1440		68	72	71	018.56
B1		0.030	1.500	1480		68	71	70	018.75
2		0.030	1.020	1430		68	70	69	018.51
3		0.030	1.000	1481		68	72	70	018.81
4		0.030	1.000	1470		68	71	70	018.71
C1		0.020	1.900	1430		68	72	71	015.51
2		0.030	1.030	1427		68	73	71	018.50
3		0.030	1.020	1442		68	73	71	018.57
4		0.030	1.020	1442		68	72	71	018.57
D1		0.020	1.400	1380		68	72	71	014.91
2		0.020	0.700	1388		68	71	70	014.94
3		0.020	0.700	1362		68	68	68	014.92
4	366.285	0.020	0.700	1371		68	69	68	014.88
Average:									
	Vm	ΔP	ΔH	***ts	tbox	tl	t 1 (in)	t 2 (out)	vs
	36.282	0.027	1.117	1433	not done	68	71.44	70.13	17.47

*** SCEC took their thermocouple readings of the first point of each port too early (when they changed ports, the thermocouple cooled down to c.a. 300-500 °F). I had to correct the temperatures at the beginning of each port change. Their temperatures were too low. To correct for this, I gave the first point of each port the average of the previous three temperatures.

METER BOX PARAMETERS: Box ID = <u>NUTECH</u> $\Delta H@$ = _____ Y = <u>0.9766</u>		NOZZLE & PROBE: Dn = <u>0.630</u> in An = <u>0.3117</u> in ² Cp = <u>0.840</u>		MISCELLANEOUS: Maximum vacuum = <u>5.0</u> in. Hg. Circular stack (Y/N) = <u>YES</u> Silica gel (Y/N) = <u>YES</u>	
VOLUME: start leak rate = <u>0.000</u> cfm Pass/Fail <u>PASS</u> final leak rate = <u>0.000</u> cfm Pass/Fail <u>PASS</u> Vm <u>36.282</u> ft ³		PRESSURES: Pbar = <u>29.85</u> in Hg Pg = <u>0.00</u> in H ₂ O Vpw @ ts = <u>29.9200</u> in Hg Vpw @ ti = <u>N/A</u> in Hg		LABORATORY DATA: mn(front) = <u>0.00322</u> g CO ₂ = <u>7.92</u> % mn(back) = <u>0.00000</u> g O ₂ = <u>11.69</u> % mn(total) = <u>0.00322</u> g CO = <u>0.00</u> % Vlc <u>80.80</u> ml N ₂ = <u>80.39</u> %	
STACK PARAMETERS: Ds = <u>3.50</u> ft Length = <u>3.50</u> ft As = <u>12.25</u> ft ²		TIME: ϕ = <u>60.0</u> min tn = <u>16</u> points s = <u>3.8</u> min/pt		TEMPERATURES: t1 = <u>71.44</u> °F ti = <u>68</u> °F t2 = <u>70.13</u> °F tbox = <u>not done</u> °F tm = <u>70.78</u> °F ts = <u>1433</u> °F	

Balboa Park (Run #1) on 3/30/92

P.O. #: none TEST#: 92090.1

SAN DIEGO AIR POLLUTION CONTROL DISTRICT, 9150 CHESAPEAKE DRIVE, SAN DIEGO, CA 92123

PARTICULATE TEST LABORATORY ANALYSIS DATA SHEET

TEST SITE: Balboa Park
2850 Pershing Dr.
San Diego, CA

TEST WITNESS - RUN #1

TEST #: 92090.1

P.O.#: none

TEST DATE: 3/30/92

LAB ANALYSIS BY: Russ Logan (of SCEC)

DATE: 4/21/92

LAB REPORT BY: Russ Logan (of SCEC)

DATE: 4/21/92

REVIEWED BY: David Shina (of SDAPCD)

DATE: 7/8/92

(1) IMPINGER VOLUMES

	FINAL WGT.	INIT WGT.	NET WGT.
#1	650.00 g	597.00 g	53.00 g
#2	614.00 g	612.40 g	1.60 g
#3	486.40 g	485.80 g	0.60 g
#4	708.10 g	700.80 g	7.30 g
#5	g	g	g

Was silica gel used (Y/N) ?= ☒ yTotal impinger charge= mlTotal weight collected= gTotal volume collected, vic= ml**(2) BLANKS**

							STANDARDS				
A	B	C	D	E	F	G	H	I	J	K	L
LOCATION	SOLVENT	ID	END WGT g	INIT WGT g	NET WGT. (E-F) g	RINSES ml	g/ml (G/D)	% (H*100)	ppm (H*10*6)	PASS FAIL	LIMITS
BLANK	ACETONE	E9	99.63435	99.63420	0.00015	100.00	0.0000015	0.0001500	1.50	P	0.0010% = 10ppm
BLANK	WATER	E14	96.75430	96.75430	0.00000	100.00	0.0000000	0.0000000	0.00	P	0.0004% = 4ppm

(3) WEIGHTS & RINSES

a	b	c	d	e	f	g	h	i	j	k
LOCATION	SOLVENT	ID	END WGT g	INIT. WGT g	NET WGT. (e-f) g	RINSES ml	SOLV. WGT (g*H) g	WGT (corr) (f-h) g	ALICUOTS g	Totals (ΣSubtotals(i+j)) g
FRONT	ACETONE									
FRONT	WATER									
FRONT	TOTAL	*								
FRONT	FILTER	G15	0.51660	0.51660	0.00000	N/A	N/A	0.000000	N/A	
FRONT	Subtotals (Σcolumn)=							0.00000		0.00000 g
BACK	ACETONE									
BACK	WATER									
BACK	TOTAL	**E4	99.81770	99.81140	0.00630	***N/A	0.000000	0.006300	0.01086	
BACK	FILTER	N/A								
BACK	Subtotals (Σcolumn)=							0.00630	0.01086	0.01716 g
TOTAL	Totals = (Σsubtotals - Σcolumn (if front & back))=									0.01716 g

* SCEC broke the probe/nozzle; so NO particulate could be analyzed for in the front half.

** For the BACK HALF totals, SCEC did NOT allow the beakers to come to a constant weight and they took an incorrect average weight. To get a weight, I took the last recorded weight and deemed it the "official average" weight.

*** SCEC did not wash out the BACK half with acetone, so the SOLV. WGT. contribution will be zero.

CONTRACTOR TEST REPORT

CONTRACTOR TEST REPORT

SAN DIEGO AIR POLLUTION CONTROL DISTRICT
MONITORING AND TECHNICAL SERVICES
9150 CHESAPEAKE DRIVE
SAN DIEGO, CA 92123

NITROGEN OXIDES, CARBON MONOXIDE, PARTICULATE,
AND SULFUR EMISSIONS SUMMARY REPORT

SITE: Arizona Street Flare

P/O NUMBER: 56896 and 59383 JOB NO: T1482-1
TEST DATE: 3/30/92

EQUIPMENT: Arizona Street Landfill Gas Collection and
Incineration System

REPORT BY: *R.P. Logan* DATE: 5/14/92
R.P. Logan - SCEC

APCD PERSONNEL: Janet Cawyer/David Shina

SITE PERSONNEL: Ray Purtee

APPROVED BY: *Justin H. Hall* DATE: 10/12/92

CALCULATIONS:**TEMPERATURES:**

01)	$t_s = (\sum t_s(n))/\text{total } n's$	1433 °F
02)	$T_s = t_s$	1893 °R
03)	$t_m = (\sum ((t_1(n)+t_2(n))/2))/\text{total } n's = (t_1+t_2)/2$	71 °F
04)	$T_m = (t_1+t_2) + 460$	531 °R
05)	$t_i = (\sum t_i(n))/\text{total } n's$	68 °F
06)	T_{std}	528 °R

PRESSURES:

07)	$P_{bar} = ((P @ S.L.) + (\text{ft. above S.L.} \cdot (-0.1 \text{ in Hg}/100\text{ft})))$	29.85 in Hg
08)	$P_g = \text{read from pressure sensing device}$	0.00 in H ₂ O
09)	$P_s = P_{bar} + (P_g/13.6)$	29.85 in Hg
10)	ΔH	1.117 in H ₂ O
11)	$P_m = P_{bar} + (\Delta H/13.6)$	29.93 in Hg
12)	P_{std}	29.92 in Hg

VOLUME:

13)	$V_m = V_m(\text{end}) - V_m(\text{begin})$	36.282 ft ³
14)	Y	0.9764
15)	$V_m' = V_m \cdot Y$	35.433 ft ³
16)	$V_{pw} @ t = \text{from appendix}$	N/A in Hg
17)	$\text{corr } V_{wm} = (((V_m' \cdot V_{pw} @ \text{imp}/P_s) \cdot P_m \cdot T_{std})/(T_m \cdot P_{std}))$	0.0000 ft ³
18)	$V_m \text{ std} = [(V_m' \cdot (T_{std}/T_m) \cdot (P_m/P_{std})) - \text{corr } V_{wm}]$	35.262 ft ³
19)	$V_{ic} = (\sum \text{Volume of impingers})$	80.80 ml
20)	ρ	0.002019 lb/ml
21)	R	21.85 in Hg-ft ³ /°R-lb-mo
22)	M_{wH_2O}	18.00 g/g-mo
23)	$V_w \text{ std} = (((V_{ic} \cdot \rho \cdot R \cdot T_{std})/(P_{std} \cdot M_{wH_2O})) + \text{corr } V_{wm})$	3.8138 ft ³

MOISTURE:

24)	$B_{ws}(1) = (V_w \text{ std}/(V_w \text{ std} + V_m \text{ std})) \cdot 100$	9.76 %
25)	$V_{pw} @ t_s = \text{from appendix}$	29.92 in Hg
26)	$B_{ws}(2) = ((V_{pw} @ t_s)/P_s) \cdot 100$	100.23 %
27)	$B_{ws} = \text{lower value of equation 24 or 26}$	9.76 %

MOLECULAR WEIGHT:

28)	%O ₂	11.69 %
29)	%CO ₂	7.92 %
30)	%N ₂ -inerts+%CO	80.39 %
31)	$M_d = [0.440(\%CO_2)] + [0.320(\%O_2)] + [0.280(\%N_2 + \text{inerts} + \%CO)]$	29.73 g/g-mole
32)	$M_s = M_d \cdot (1 - B_{ws}) + 18.0 \cdot B_{ws}$	28.59 g/g-mole

FLOW:

33)	ΔP	0.0267 in H ₂ O
34)	C_p	0.240
35)	$v_s = 85.49 \cdot C_p \cdot [((T_s \cdot \Delta P)/(P_s \cdot M_s))]^{.5}$	17.475 ft/sec
36)	$A_s = 3.14 \cdot [(D_s)^2/4]$	12.260 ft ²
37)	$Q_s = (v_s) \cdot A_s \cdot 60$	12844 acfm
38)	$Q_{std} = 17.64 \cdot Q_s \cdot (1 - B_{ws}) \cdot P_s/T_s$	3323 dscfm

EMISSIONS:**FRONT HALF**

39)	$m_n (\text{front})$	0.00322 g
40)	$C_s (\text{front}) = (15.45 \cdot m_n (\text{front})/V_m \text{ std})$	0.00131 grains/dscf
41)	$C_s(12\%, \text{front}) = (12/\%CO_2) \cdot C_s(\text{front})$	0.002 grains/dscf
42)	$E (\text{front}) = (Q_{std} \cdot C_s(12\%, \text{front}))$	0.04 lb/hr

BACK HALF

43)	$m_n (\text{back})$	0.00000 g
44)	$C_s (\text{back}) = (15.45 \cdot m_n (\text{back})/V_m \text{ std})$	0.00000 grains/dscf
45)	$C_s(12\%, \text{back}) = (12/\%CO_2) \cdot C_s(\text{back})$	0.000 grains/dscf
46)	$E (\text{back}) = (Q_{std} \cdot C_s(12\%, \text{back}))$	0.00 lb/hr

TOTAL

47)	$m_n (\text{total}) = m_n(\text{front}) + m_n(\text{back})$	0.00322 g
48)	$C_s (\text{total}) = (15.45 \cdot m_n (\text{total})/V_m \text{ std})$	0.00131 grains/dscf
49)	$C_s(12\%, \text{total}) = (12/\%CO_2) \cdot C_s(\text{total})$	0.002 grains/dscf
50)	$E (\text{total}) = (Q_{std} \cdot C_s(12\%, \text{total}))$	0.04 lb/hr
51)	$E.A. = [(\%O_2 \cdot .5(\%CO) \cdot 100)/[0.264(\%N_2) - (\%O_2) - 0.5(\%CO)]]$	122.63 %

ISOKINETICS:

52)	D_w	0.630 in
53)	$A_n = 3.14 \cdot [(D_n)^2/4]$	0.3117 in ²
54)	$L = 0.450 \cdot (T_s \cdot V_m \text{ std}/P_s \cdot V_s \cdot A_n \cdot (1 - B_{ws}))$	183.20 % = 183 %

Balboa Park (Run #2) on 3/30/92

SAN DIEGO AIR POLLUTION CONTROL DISTRICT, 9150 CHESAPEAKE DRIVE, SAN DIEGO, CA 92123

P.O. #: none TEST #: 92090.2

PARTICULATE TEST LABORATORY ANALYSIS DATA SHEET

TEST SITE: Balboa Park
2850 Pershing Dr.
San Diego, CA

TEST WITNESS - RUN #2

TEST #: 92090.2

P.O. #: none

TEST DATE: 3/30/92

LAB ANALYSIS BY: Russ Logan (of SCEC)

DATE: 4/21/92

LAB REPORT BY: Russ Logan (of SCEC)

DATE: 4/21/92

REVIEWED BY: David Shina (of SDAPCD)

DATE: 7/8/92

(1) IMPINGER VOLUMES

	FINAL WGT.	INIT WGT.	NET WGT.
#1	657.80 g	587.60 g	70.20 g
#2	612.10 g	610.10 g	2.00 g
#3	488.80 g	486.40 g	2.40 g
#4	714.30 g	708.10 g	6.20 g
#5	g	g	g

Was silica gel used (Y/N) ?= ☒ y

Total impinger charge= ml

Total weight collected= g

Total volume collected/Vic= ml

(2) BLANKS

A	B	C	D	E	F	G	STANDARDS				
LOCATION	SOLVENT	ID	END WGT g	INIT WGT g	NET WGT. g (E-F)	RINSES ml (G/D)	H g/ml (G/D)	I % (H*100)	J ppm (H*10*6)	K PASS FAIL	L LIMITS
BLANK	ACETONE	E9	99.63435	99.63420	0.00015	100.00	0.0000015	0.0001500	1.50	P	0.0010% = 10ppm
ANK	WATER	E14	96.75430	96.75430	0.00000	100.00	0.0000000	0.0000000	0.00	P	0.0004% = 4ppm

(3) WEIGHTS & RINSES

a	b	c	d	e	f	g	h	i	j	k
LOCATION	SOLVENT	ID	END WGT g	INIT. WGT g	NET WGT. g (e-f)	RINSES ml	SOLV. WGT g (g*h)	WGT (corr) g (f-h)	ALICUOTS g	Totals g (Σ Subtotals (i+j))
FRONT	ACETONE									
FRONT	WATER									
FRONT	TOTAL	E17	95.88510	95.88240	0.00270	**50	0.000075	0.002625	0.00000	
FRONT	FILTER	**G16	0.51900	0.51840	0.00060	N/A	N/A	0.000600	N/A	
FRONT	Subtotals (Σ column) =							0.00322	0.00000	0.00322 g
BACK	ACETONE									
BACK	WATER									
BACK	TOTAL	***E2	97.28090	97.28160	0.00000	****N/A	0.000000	0.000000	0.00000	
BACK	FILTER	N/A								
BACK	Subtotals (Σ column) =							0.00000	0.00000	0.00000 g
TOTAL	Totals = (Σ Subtotals = Σ column k (front & back)) =									0.00322 g

* For the FRONT HALF totals, SCEC did NOT allow the beakers to come to a constant weight and they took an incorrect average weight. To get a weight, I took the last recorded weight and deemed it the "official average" weight.

** SCEC used only 50 ml of acetone for the FRONT half rinses. The water is blank is 0 ppm, so there will be no SOLV. WGT. value.

*** SCEC did not allow the filter to come to a constant weight. To get a weight, I used the last recorded weight.

SCEC took an incorrect average weight. When I corrected for this, E2's END WEIGHT was more than the tare, INITIAL WEIGHT. Because of this, I had to make the NET WEIGHT zero, and this is why there is NO particulate contribution from the back half.

**** SCEC did not wash out the BACK half with acetone, so the SOLV. WGT. contribution will be zero

COMPANY: ARIZONA STREET
 DATE: 3/30/92
 UNIT: FLARE
 REPORT #: T1482-1

RUN #2
 @ 68°F
 EPA METHOD 5/8

PARTICULATE RESULTS:	net mg	gr/dscf	gr/scf	gr/dscf @ 12% CO2	lbs/hr
Probe & Nozzle:	4.9	0.002140	0.001932	0.003243	0.06
Filter:	0.7	0.000305	0.000276	0.000463	0.01
Condensables:	8.33	0.003639	0.003284	0.005513	0.11
Total:	13.93	0.006085	0.005492	0.009220	0.18

N BaCl = 0.00971

SULFATE RESULTS:	Vol aliq	Vt	gr/dscf	gr/scf	gr/dscf @ 12% CO2	lbs/hr
Probe & Nozzle:	7	0	0	0	0	0
Filter:	10	0	0	0	0	0
Condensables:	34	0.18	0.001259	0.001136	0.001907	0.04
Total:			0.001259	0.001136	0.001907	0.04

ADDITIONAL DATA:

TIME		%O2	%CO2	%H2O	Vm(std)	SDCFM
start	finish					
1403	1508	11.69	7.92	9.74	35.25	3402



PLANT Arizona Test Ty Garb 107005 FIELD TEST DATA SHEET

Date 3/30/92
Test Location Garb
Run Number #2
Stack Diameter 42" x 42"
Operator TJS
Filter No. 616 0.588 Nozzle No./Size 0.587
Start Time 1403
Barometric Pressure 29.85
Static In. wg. 0.00
Probe Type/Length 6' H20 Probe
Pitot Coefficient 0.84
Meter Box No. Adv Tech

Impinger Volumes/Weights					Gas Composition		
Contents	Final	Initial	Net	Time	CO2	O2	CO
H2O	659.8	587.6	72.2		8.2	12.0	
H2O	612.1	602.1	2.0		7.92	11.67	
H2O	488.8	486.4	2.4				
Silica Gel	714.5	708.1	6.2				
				Leak Rate	cfm		"Hg
				Initial			
				Final			
		Total	40.8		1.00	20"	
					0.00	20"	

Sample Point	Time	ΔP In wg	ΔH In wg	Gas Meter Volume Ft ³	Temperature °F				Stack	Probe	Gas Meter		Pump Vacuum In. Hg	√ΔP	Comments
					Oven	Imp.	In	Out			In	Out			
4	0:00	0.02	1.55	336.003			71	70	300					5	
3	3:45	0.03	1.00	332.5			73	71	1460					5	
2	7:00	0.03	1.01	334.6			72	70	1452					5	
1	11:15	0.03	1.02	336.55			72	71	1440					5	1.2 = 36.28
1	15:00	0.03	1.8	339			71	70	606					5	ΔP = 0.027
1	18:45	0.03	1.02	341			70	69	1430					5	ΔH = 0.885
1	22:00	0.02	1.00	343.5			72	70	1491					5	1.117
1	26:15	0.03	1.00	345			71	70	1470					5	1.2545
1	30:00	0.03	1.9	348			72	71	554					5	1.2 = 70.93
3	33:45	0.03	1.03	351			73	71	1477					5	Duration = 6 min
2	37:30	0.03	1.02	353			73	71	1442					5	
1	41:15	0.03	1.02	356			72	71	1442					5	
1	45:00	0.02	1.1	358			71	70	1442					5	

Position	02	CO
	01	119

[illegible][illegible]

Client: SOAD & ALGHAM ST.

Report #: T1452

Test Date: 3/30/92

Analyst: PC

Site: COAST-FL-245

Run No: 2

GRAVIMETRIC ANALYSIS

Fraction: Probes and Nozzle Washings REF: ST17

Date: <u>4/11</u>	Date:	Date:	* NO amt ± AVERAGE 95.8831 grms. 95.8824 grms. NET: 49 mg.
Time: <u>13:15</u>	Time:	Time:	
#1	#2	#3	
Final: <u>95.890</u>	<u>95.8858</u>	<u>95.8851</u>	
Tare:			

Fraction: Filter

Filter No: 616

Date:	Date:	Date:	AVERAGE 0.5191 grms. 0.5184 grms. NET: 0.7 mg.
Time:	Time:	Time:	
#1	#2	#3	
Final: <u>0.5200</u>	<u>0.5182</u>	<u>0.5190</u>	
Tare:			

Fraction: Condensables

Aliquot: 200 Total Sample: 340 ml

Date: <u>4/14</u>	Date:	Date:	AVERAGE 97.2865 grms. 97.2816 grms. NET: 49 mg.
Time: <u>1357</u>	Time:	Time:	
#1	#2	#3	
Final: <u>97.2978</u>	<u>97.2808</u>	<u>97.2810</u>	
Tare:			

Fraction: Condensable Organics

TOTAL:

Acetone Blank 100 ml

Date: <u>4/13</u>	Date: <u>4/14</u>	Date:	AVERAGE 99.6343 grms. 99.6342 grms. NET: 0.01 mg.
Time:	Time:	Time:	
#1	#2	#3	
Final: <u>99.6341</u>	<u>99.6346</u>		
Tare:			

DO they mix front ac & H₂O

FIELD DATA & DATA SUMMARY:

Trav. Pt	Vm (ft ³)	ΔP (in H ₂ O)	ΔH (in H ₂ O)	Stack Temp (°F)	Box Temp (°F)	Imp Temp (°F)	t 1 (in) (°F)	t 2 (out) (°F)	velocity (ft/sec)
	367.164								
A1		0.020	1.330	1445		68	73	71	015.14
2		0.030	1.020	1445		68	73	71	018.55
3		0.030	1.010	1445		68	71	69	018.55
4		0.020	0.690	1405		68	70	69	014.98
B1		0.030	1.890	1470		68	71	70	018.67
2		0.040	1.320	1482		68	70	70	021.62
3		0.030	1.000	1470		68	71	70	018.67
4		0.030	1.000	1464		68	68	68	018.64
C1		0.030	2.400	1395		68	69	68	018.30
2		0.020	0.690	1391		68	69	69	014.93
3		0.020	0.680	1406		68	68	68	014.99
4		0.030	0.690	1395		68	67	67	018.30
D1		0.020	1.300	1440		68	68	68	015.12
2		0.020	0.670	1454		68	67	67	015.18
3		0.030	1.010	1431		68	67	67	018.48
4	400.344	0.030	1.000	1452		68	67	67	018.58
Average:									
	Vm	ΔP	ΔH	***ts	tbox	ti	t 1 (in)	t 2 (out)	vs
	33.180	0.027	1.106	1437	not done	68	69.19	68.56	17.42

*** SCEC took their thermocouple readings of the first point of each port too early (when they changed ports, the thermocouple cooled down to c.a. 300-500 °F). I had to correct the temperatures at the beginning of each port change. Their temperatures were too low. To correct for this, I gave the first point of each port the average of the previous three temperatures.

METER BOX PARAMETERS: Box ID = <u>NUTECH</u> $\Delta H@$ = _____ Y = <u>0.9766</u>		NOZZLE & PROBE: Dn = <u>0.587</u> in An = <u>0.2706</u> in ² Cp = <u>0.840</u>		MISCELLANEOUS: Maximum vacuum = <u>5.0</u> in. Hg. Circular stack (Y/N) = <u>YES</u> Silica gel (Y/N) = <u>YES</u>	
VOLUME: start leak rate = <u>0.000</u> cfm Pass/Fail <u>PASS</u> final leak rate = <u>0.000</u> cfm Pass/Fail <u>PASS</u> Vm <u>33.180</u> ft ³		PRESSURES: Pbar = <u>29.85</u> in Hg Pg = <u>0.00</u> in H ₂ O Vpw @ ts = <u>29.9200</u> in Hg Vpw @ ti = <u>N/A</u> in Hg		LABORATORY DATA: mn(front) = <u>0.004675</u> g CO ₂ = <u>7.81</u> % mn(back) = <u>0.001960</u> g O ₂ = <u>11.70</u> % mn(total) = <u>0.00664</u> g CO = <u>0.00</u> % Vlc <u>65.10</u> ml N ₂ = <u>80.49</u> %	
STACK PARAMETERS: Ds = <u>3.50</u> ft Length = <u>3.50</u> ft As = <u>12.25</u> ft ²		TIME: ϕ = <u>60.0</u> min tn = <u>16</u> points s = <u>3.8</u> min/pt		TEMPERATURES: t1 = <u>69.19</u> °F ti = <u>68</u> °F t2 = <u>68.56</u> °F tbox = <u>not done</u> °F tm = <u>68.88</u> °F ts = <u>1437</u> °F	

SOURCE TEST OF PARTICULATE EMISSIONS TO THE ATMOSPHERE

TEST SITE: Balboa Park Landfill Flare
 2850 Pershing Dr.
 San Diego, Ca

TEST WITNESS - RUN #3

TEST #: 92090.3

P.O.#: none

TEST DATE: 3/30/92

Type of plant (Asphalt / Perlite / Combustion): **COMBUSTION**

UNIT TESTED: INCINERATOR

EQUIPMENT: LANDFILL FLARE

TESTED BY: Russ Logan & Ted Jackman of SCEC

SITE PERSONNEL: Ray Purtee

DATE: 3/30/92

APCD ENGINEER: Archi de la Cruz

DATE: 3/30/92

LAB ANALYSIS BY: SCEC

DATE: 3/30/92

REPORT BY: SCEC (Russ Logan)

DATE: 4/21/92

REVIEWED BY: David N. Shina

DATE: 4/21/92

APPROVED BY:

DATE: 7/9/92

JUDITH LAKE, CHIEF OF MONITORING

This report has been reviewed and found to be representative of the testing that was performed.

SDAPCD RULES

TEST	LIMIT	MEASURED	PASS/FAIL
E 53 SPECIFIC CONT.	0.10 gr/dscf	0.005 gr/dscf	NON-EXCEEDANCE

TEST RESULTS SUMMARY:

ITEM	I	Cs(12%)	E
UNITS	%	gr/dscf	lbs/hr
VALUE	108	0.0049	0.09

ENGINEERING SUMMARY

Qstd	TYPE OF FUEL	LOAD	RATE
dscfm		Tons/Hr	Tons
3246			

TEST PARAMETERS:

SYSTEM DESCRIPTION:

Landfill gas is sucked through the piping of this system. The landfill gas is constantly being burned off by the flare combustion system. The flare is at the bottom of the incinerator stack. The sampling points are near the top of the stack. The particulate emissions from this process are the subject of the report.

PROCEDURES:

The procedures and equipment utilized in these tests are based on EPA New Source Performance Standards Method 5. The sampling train utilized a front-end filter (fig. 1)

CALCULATIONS

All equations are from EPA CFR 40, July 1, 1991, Parts 53-60, Appendix A, Methods 1-5 inclusive.

PARTICULATE SAMPLING:

The test consisted of sampling at 16 traverse points, 4 from each of 4 sample ports (fig.2), collected from 84 inches below the stack (fig.3). All field data was transferred to the computer printout. All calculations were done by the computer and the emissions were compared to rule 53b of the SDAPCD.

ANALYSES:

Gas: A CEM analysis was performed by SCEC.

Particulate: All procedures follow EPA guidelines, except where noted in the SDAPCD QA manual.

EQUIPMENT:

All testing and analysis equipment was calibrated according to EPA guidelines and done by SCEC.

CALCULATIONS:**TEMPERATURES:**

01)	$t_s = (\sum t_s(n))/\text{total } n's$	1437 °F
02)	$T_s = t_s + 460$	1897 °R
03)	$t_m = (\sum ((t_1(n) + t_2(n))/2))/\text{total } n's = (t_1 + t_2)/2$	69 °F
04)	$T_m = (t_1 + t_2)/2 + 460$	529 °R
05)	$t_i = (\sum t_i(n))/\text{total } n's$	68 °F
06)	T_{std}	528 °R

PRESSURES:

07)	$P_{bar} = \{(P @ \text{S.L.}) + [\text{ft. above S.L.} \cdot (-0.1 \text{ in Hg}/100\text{ft})]\}$	29.85 in Hg
08)	$P_g = \text{read from pressure sensing device}$	0.00 in H ₂ O
09)	$P_s = P_{bar} + (P_g/13.6)$	29.85 in Hg
10)	ΔH	1.106 in H ₂ O
11)	$P_m = P_{bar} + (\Delta H/13.6)$	29.93 in Hg
12)	P_{std}	29.92 in Hg

VOLUME:

13)	$V_m = V_m(\text{end}) - V_m(\text{begin})$	33.180 ft ³
14)	Y	0.9766
15)	$V_m' = V_m \cdot Y$	32.404 ft ³
16)	$V_{pw} @ t = \text{from appendix}$	N/A in Hg
17)	$\text{corr } V_{wm} = \{[(V_m' \cdot V_{pw} @ \text{imp}/P_s) \cdot P_m \cdot T_{std}]/(T_m \cdot P_{std})\}$	0.0000 ft ³
18)	$V_{m \text{ std}} = \{V_m' \cdot [T_{std}/T_m] \cdot [P_m/P_{std}]\} - \text{corr } V_{wm}$	32.362 ft ³
19)	$V_{ic} = (\sum \text{Volume of impingers})$	65.10 ml
20)	ρ	0.002010 lb/ml
21)	R	21.85 in Hg-ft ³ /°R-lb-mo
22)	M_{wH_2O}	18.00 g/g-mo
23)	$V_w \text{ std} = \{[(V_{ic} \cdot \rho \cdot R \cdot T_{std})/(P_{std} \cdot M_{wH_2O})] + \text{corr } V_{wm}\}$	3.0727 ft ³

MOISTURE:

24)	$B_{ws}(1) = (V_w \text{ std})/(V_w \text{ std} + V_m \text{ std}) \cdot 100$	8.67 %
25)	$V_{pw} @ t_s = \text{from appendix}$	29.92 in Hg
26)	$B_{ws}(2) = \{[(V_{pw} @ t_s)/P_s] \cdot 100\}$	100.23 %
27)	$B_{ws} = \text{lower value of equation 24 or 26}$	8.67 %

MOLECULAR WEIGHT:

28)	%O ₂	11.70 %
29)	%CO ₂	7.81 %
30)	%N ₂ +inerts+%CO	80.49 %
31)	$M_d = [0.440(\%CO_2)] + [0.320(\%O_2)] + [0.280(\%N_2 + \text{inerts} + \%CO)]$	29.72 g/g-mole
32)	$M_s = M_d \cdot [(1 - B_{ws}) + 18.0 \cdot (B_{ws})]$	28.70 g/g-mole

FLOW:

33)	ΔP	0.0266 in H ₂ O
34)	C_p	0.240
35)	$v_s = 85.49 \cdot C_p \cdot \{[(T_s \cdot \Delta P)/(P_s \cdot M_s)]^{.5}\}$	17.419 ft/sec
36)	$A_s = 3.14 \cdot [(D_s)^2/4]$	12.250 ft ²
37)	$Q_s = (v_s) \cdot A_s \cdot 60$	12803 acfm
38)	$Q_{std} = 17.64 \cdot Q_s \cdot [(1 - B_{ws}) \cdot P_s/T_s]$	3245 dscfm

EMISSIONS:**FRONT HALF**

39)	$m_n (\text{front})$	0.00468 g
40)	$C_s (\text{front}) = 15.43 \cdot m_n (\text{front})/V_m \text{ std}$	0.00223 grains/dscf
41)	$C_s(12\%, \text{front}) = (12/\%CO_2) \cdot C_s (\text{front})$	0.003 grains/dscf
42)	$E (\text{front}) = (0.0057) \cdot (Q_{std}) \cdot C_s (\text{front})$	0.06 lbs/hr

BACK HALF

43)	$m_n (\text{back})$	0.00196 g
44)	$C_s (\text{back}) = 15.43 \cdot m_n (\text{back})/V_m \text{ std}$	0.00093 grains/dscf
45)	$C_s(12\%, \text{back}) = (12/\%CO_2) \cdot C_s (\text{back})$	0.001 grains/dscf
46)	$E (\text{back}) = (0.0057) \cdot (Q_{std}) \cdot C_s (\text{back})$	0.03 lbs/hr

TOTAL

47)	$m_n (\text{total}) = m_n (\text{front}) + m_n (\text{back})$	0.00664 g
48)	$C_s (\text{total}) = 15.43 \cdot m_n (\text{total})/V_m \text{ std}$	0.00316 grains/dscf
49)	$C_s(12\%, \text{total}) = (12/\%CO_2) \cdot C_s (\text{total})$	0.005 grains/dscf
50)	$E (\text{total}) = (0.0057) \cdot (Q_{std}) \cdot C_s (\text{total})$	0.09 lbs/hr
51)	$E.A. = \{[(\%O_2 \cdot 5(\%CO) \cdot 100)/[0.264(\%N_2) - (\%O_2) - 0.5(\%CO)]]\}$	122.52 %

ISOKINETICS:

52)	D_n	0.587 in
53)	$A_n = 3.14 \cdot [(D_n)^2/4]$	0.2706 in ²
54)	$I = 0.450 \cdot (T_s \cdot V_m \text{ std})/P_s \cdot V_s \cdot A_n \cdot [(1 - B_{ws})]$	108.34 % = 108 %

SAN DIEGO AIR POLLUTION CONTROL DISTRICT, 9150 CHESAPEAKE DRIVE, SAN DIEGO, CA 92123

PARTICULATE TEST LABORATORY ANALYSIS DATA SHEET

TEST SITE: Balboa Park Landfill flare
2850 Pershing Dr.
San Diego, CA

TEST WITNESS - RUN #3

TEST #: 92090.3

P.O.#: none

LAB ANALYSIS BY: Russ Logan (of SCEC)

TEST DATE: 3/30/92

LAB REPORT BY: Russ Logan (of SCEC)

DATE: 4/21/92

REVIEWED BY: David Shina (of SDAPCD)

DATE: 4/21/92

DATE: 7/8/92

(1) IMPINGER VOLUMES

	FINAL WGT.	INIT WGT.	NET WGT.
#1	658.00 g	597.10 g	60.90 g
#2	613.60 g	612.10 g	1.50 g
#3	487.50 g	488.80 g	-1.30 g
#4	718.30 g	714.30 g	4.00 g
#5	g	g	g

Was silica gel used (Y/N) ?= ☒ y

Total impinger charge= 200.00 ml

Total weight collected= 65.10 g

Total volume collected, Vlc= 65.10 ml

(2) BLANKS

A	B	C	D	E	F	G	STANDARDS				
LOCATION	SOLVENT	ID	END WGT g	INIT WGT g	NET WGT. g (E-F)	RINSES ml (G/D)	H g/ml (H*100)	I %	J ppm (H*10*6)	K PASS FAIL	L LIMITS
BLANK	ACETONE	E9	99.63435	99.63420	0.00015	100.00	0.0000015	0.0001500	1.50	P	0.0010% = 10ppm
ANK	WATER	E14	96.75430	96.75430	0.00000	100.00	0.0000000	0.0000000	0.00	P	0.0004% = 4ppm

(3) WEIGHTS & RINSES

a	b	c	d	e	f	g	h	i	j	k
LOCATION	SOLVENT	ID	END WGT g	INIT. WGT g	NET WGT. g (e-f)	RINSES ml	SOLV. WGT g (g*h)	WGT (corr) g (i-h)	ALIQOTS g	Totals (ΣSubtotals(i+j)) g
FRONT	ACETONE									
FRONT	WATER									
FRONT	TOTAL	*E20	99.07780	99.07570	0.00210	**50	0.000075	0.002025	0.00000	
FRONT	FILTER	G17	0.51905	0.51640	0.00265	N/A	N/A	0.002650	N/A	
FRONT	Subtotals (Σcolumn)=							0.00467	0.00000	0.004675 g
BACK	ACETONE									
BACK	WATER									
BACK	TOTAL	***E18	96.32470	96.32330	0.00140	****0.00	0.000000	0.001400	0.00056	
BACK	FILTER	N/A								
BACK	Subtotals (Σcolumn)=							0.00140	0.00056	0.001960 g
TOTAL	Totals = (Σsubtotals - Σcolumn k(front & back))=									0.00664 g

* For the FRONT HALF totals, SCEC did NOT allow the beakers to come to a constant weight and they took an incorrect average weight. To get a weight, I took the last recorded weight and deemed it the "official average" weight.

** SCEC used only 50 mls of acetone for the FRONT half rinses. The water is blank is 0 ppm, so there will be no SOLV. WGT. value.

*** SCEC took an incorrect average weight, so I had to correct for it.

**** SCEC did not wash out the BACK half with acetone, so the SOLV. WGT. contribution will be zero

SAN DIEGO AIR POLLUTION CONTROL DISTRICT
MONITORING AND TECHNICAL SERVICES
9150 CHESAPEAKE DRIVE
SAN DIEGO, CA 92123

NITROGEN OXIDES, CARBON MONOXIDE, PARTICULATE,
AND SULFUR EMISSIONS SUMMARY REPORT

SITE: Arizona Street Flare

P/O NUMBER: 56896 and 59383 JOB NO: T1482-1
TEST DATE: 3/30/92

EQUIPMENT: Arizona Street Landfill Gas Collection and
Incineration System

REPORT BY:  DATE: 5/14/92
R.P. Logan - SCEC

APCD PERSONNEL: Janet Cawyer/David Shina

SITE PERSONNEL: Ray Purtee

APPROVED BY:  DATE: 10/12/92

CONTRACTOR TEST REPORT

COMPANY: ARIZONA STREET
 DATE: 3/30/92
 UNIT: FLARE
 REPORT #: T1482-1

RUN #3
 @ 68°F
 EPA METHOD 5/8

PARTICULATE RESULTS:

Probe & Nozzle:	net mg	gr/dscf	gr/scf	gr/dscf @ 12% CO2	lbs/hr
Filter:	5.3	0.002522	0.002304	0.003875	0.07
Condensables:	2.6	0.001237	0.001130	0.001901	0.03
	1.26	0.000599	0.000547	0.000921	0.02
Total:	9.16	0.004359	0.003982	0.006697	0.12

N BaCl = 0.00971
 SULFATE RESULTS:

Probe & Nozzle:	Vol aliq	Vt	gr/dscf	gr/scf	gr/dscf @ 12% CO2	lbs/hr
Filter:	15	0	0	0	0	0
Condensables:	10	0	0	0	0	0
	28	0.24	0.001506	0.001375	0.002314	0.04
Total:			0.001506	0.001375	0.002314	0.04

ADDITIONAL DATA:

TIME	TIME	%O2	%CO2	%H2O	Vm(std)	SDCFM
start	finish					
1600	1700	11.7	7.81	8.65	32.36	3267

PLANT LANDFILL FLARE CARD Method 5 FIELD TEST DATA SHEET

Location ARIZONA ST. TEST TUN

UNIDENTIFIED

Barometric pressure 29.92

Static In. wg. 0.00

Probe Type/Length 6' 1/2" 2000

Probe Coefficient .64

Pilot Coefficient .64

Meter Box No. Nuclek CB-2

Meter No./Size 0.58

Nozzle No./Size 1/8"

Start time 6:17

Stop time 6:00

Location LANDFILL FLARE

Number 43

Diameter TJE

Operator TJE

Order No. 617 0.5164

Impinger Volumes/Weights				Gas Composition		
Contents	Final	Initial	Net	Time	CO ₂	O ₂
H ₂ O	658.0	597.1	60.90		7.81	11.7
H ₂ O	65.6	612.1	1.50			
H ₂ O	487.5	586.8	-1.30			
Silica Gel	718.3	714.3	4.00			
				Leak Rate		
				Initial		0.00
				Final		0.00
			Total			15"

Sample Point	Time	ΔP In wg	ΔH In wg	Gas Meter Volume Ft ³	Temperature of			Gas Meter In	Gas Meter Out	Imp.	Probe	Stack	Pump Vacuum In. Hg	√ΔP	Comments
					Oven	Probe	Imp.								
4	0:00	0.02	1.33	367.164				73	71			510		5	√ ~ 33.180
3	3:45	0.03	1.02	369				73	71			1445		5	ΔP = 0.027
2	7:30	0.03	1.01	371				71	69			1445		5	ΔH = 1.105
1	11:15	0.02	0.89	374				70	70			562		5	T _s = 1436.7
4	15:00	0.03	1.89	376				71	70			1482		5	T _m = 68.88
3	18:45	0.04	1.32	378				71	70			1470		5	60 min.
2	22:30	0.03	1.00	380				68	68			1464		5	
1	26:15	0.03	1.00	382				69	68			341		5	
4	30:00	0.03	2.40	385				69	69			1791		5	
	30:00	0.02	0.89	387				68	68			1791		5	

3/30/72

Barometric Pressure 29.92

Static In. wg. 0.20

Probe Type/Length 6' H2O

Pilot Coefficient 0.84

meter Box No. NU Tech

Bozzle No. 1220
Size 15/0
No. 1220

828

Impinger Volumes/Weights				Gas Composition					
Contents	F _{final}	I _{nitial}	Net	Time	CO ₂	O ₂	CO	Leak Rate cfm	H ₂
Total									
	</								

[illegible]

Client: SDAPCO - AC-100Report #: T1482Test Date: 3/30/9-Analyst: FISite: Flint, Mich.Run No: 3

GRAVIMETRIC ANALYSIS

Fraction: Probes and Nozzle Washings - 100

REF: ST17

Date:	Date:	Date:	AVERAGE
Time: #1	Time: #2	Time: #3	
Final: <u>99.02</u>	<u>99.02</u>	<u>99.02</u>	
Tare:			
			99.02 grms.
			99.0252 grms.
			NET: <u>3</u> mg.

Fraction: Filter

Filter No: 612

Date:	Date:	Date:	AVERAGE
Time: #1	Time: #2	Time: #3	
Final: <u>0.5217</u>	<u>0.5191</u>	<u>0.5190</u>	
Tare:			
			0.5190 grms.
			0.5164 grms.
			NET: <u>3</u> mg.

Fraction: Condensables

Aliquot: 200 Total Sample: 280

Date:	Date:	Date:	AVERAGE
Time: #1	Time: #2	Time: #3	
Final: <u>96.3255</u>	<u>96.3247</u>	<u>96.3247</u>	
Tare:			
			96.3253 grms.
			96.3253 grms.
			NET: <u>0.2</u> mg.
			<u>1.26</u>
			<u>2.52</u> mg.

Fraction: ~~Condensable Organics~~ Water blank 100ml.

Date: <u>4/13</u>	Date: <u>4/14</u>	Date:	AVERAGE
Time: #1	Time: #2	Time: #3	
Final: <u>96.7541</u>	<u>96.7544</u>		
Tare:			
			96.7511 grms.
			96.7543 grms.
			NET: <u>0</u> mg.


SCEC

FACSIMILE TRANSMISSION

DATE: 7-8-92TO: Davis SHWACOMPANY: SDAPCDTRANSMITTING TO TELECOPY #: (619) 694-2730FROM: RUSS LOGANTELEPHONE #: (714) 282-8240TELECOPY #: (714) 282-8247REGARDING: TARE WEIGHTSTOTAL NUMBER OF PAGES INCLUDING COVER SHEET: 2

If there is a transmission problem, please call ASAP

TRANSMISSION SENT FROM: SCEC
1582-1 N. Batavia Street
Orange, CA 92667
(714) 282-8240
FAX (714) 282-8247

COMMENTS:

Davis,Here's the Tare Weights
sheet.RussMESSAGE # 2613

EVAPORATION DISH TARE WEIGHTS

Use new anti-static gloves!

D/T	T/RH BP	4/8/92 ¹⁰⁰	4/11/92 ¹²⁰	4/12/92 ¹¹⁰	
DISH #		TARE 1	TARE 2	TARE 3	AVERAGE
E 1					
E 2		97.2815	97.2817	97.2817	97.2816
E 3		101.9300	101.9300	101.9302	101.9301
E 4		99.8116	99.8115	99.8112	99.8114
E 5		95.4200	95.4202	95.4199	95.4200
E 6		101.3355	101.3356	101.3356	101.3356
E 7		98.4943	98.4942	98.4941	98.4942
E 8					
E 9		99.6542	weight #4 99.6342 99.6536 7	99.6341	99.6342
E 10					
E 11		Henkel final			
E 12		96.8153	96.8155	96.8155	96.8154
E 13		Henkel			
E 14		96.7543	96.7543		96.7543
E 15		Henkel	final weights		
E 16					
E 17		95.8822	95.8824	95.8824	95.8824
E 18		96.3234	96.3234	96.3231	96.3233
E 19		Henkel final			
E 20		99.0757	99.0758	99.0757	99.0757
E 21					
E 22					

broken, opps!



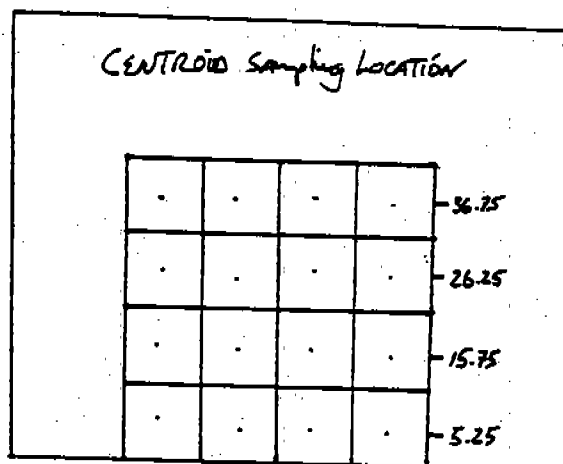
SCEC
1582-1 N. BATAVIA
ORANGE, CA 92667

FILE REF: ST12

SAMPLE POINT LOCATION DATA SHEET

FACILITY: ARIZONA STREET
PROJECT #: T-482
DATE: 3/30/92
STACK DIMENSIONS: L= 42"
W= 42"
H=

UPSTREAM DIST./
EQUIVALENT DIAMETERS 5
DOWNSTREAM DIST./
EQUIVALENT DIAMETERS 2
NO. OF SAMPLING POINTS
SAMPLING PORT DIMENSIONS:
DIA. = 3"
PROTRUSION DIST. = 3"



SAMPLE POINT	% OF STACK DIAMETER	DISTANCE FROM STACK WALL (IN.)	DISTANCE FROM SAMPLE PORT (IN.)
EACH PORT			
#1		36.75	39.75
#2		26.25	29.25
#3		15.75	18.75
#4		5.25	8.25

