



CALPINE

Note: This is a reference cited in AP 42, *Compilation of Air Pollutant Emission Factors, Volume I Stationary Point and Area Sources*. AP42 is located on the EPA web site at www.epa.gov/ttn/chief/ap42/

The file name refers to the reference number, the AP42 chapter and section. The file name "ref02_c01s02.pdf" would mean the reference is from AP42 chapter 1 section 2. The reference may be from a previous version of the section and no longer cited. The primary source should always be checked.

October 7, 1992

408.995.0505 (fax)

Scott Lutz
Supervising Air Quality Engineer
TAC Evaluation Section
BAY AREA AIR QUALITY MANAGEMENT DISTRICT
939 Ellis Street
San Francisco, California 94109

Subject: AB2588 Toxic Hot Spots Fee

Dear Mr. Lutz:

In anticipation of the adoption of regulations that would impose fees for emissions identified in Assembly Bill 2588, an emissions source test was conducted at the Agnews Cogeneration Facility, Plant #6044. As discussed in my July 30, 1992 letter to you, this test was conducted to determine the actual formaldehyde emissions. The test conducted by BEST ENVIRONMENTAL on September 15, 1992, showed the actual emissions of formaldehyde were only 17 percent of BAAQMD estimated levels. A copy of the test report is enclosed for your reference.

Enclosed is a copy of the BAAQMD Toxic Emissions Inventory dated September 3, 1992. I have corrected the inventory to include the actual emissions with a calculation showing how the number was determined. The toxic fee should be \$500 based on the current schedule.

If you have any questions, please give me a call.

Sincerely,

CALPINE CORPORATION

R. Becker

Richard A. Becker
Project Manager

RABdcb/lcp
LET1092.18

Enclosure

cc: Tom Coonrod - COPS

IF THIS REGULATION IS ADOPTED
YOUR 1991-1992 AB 2588 FEE WILL BE \$ ~~2000~~ \$500 ← SCHEDULE N

BEST ENVIRONMENTAL, INC.

5890 Foothill Boulevard
San Leandro, California 94578
(510) 278-4011 FAX (510) 278-4018

October 2, 1992

CALPINE
50 W. San Fernando St. 5th Fl.
San Jose, CA 95113

Attn: Richard Becker:

Subject: **Source emission test report regarding formaldehyde emissions from the Agnews Cogeneration Facility, San Jose, CA.**

Test Date: September 15, 1992.

Sampling Location: Sampling was conducted at the outlet stack of the steam boiler/turbine, located at 3530 Zanker Road, San Jose, CA.

Sampling Personnel: Sampling was performed by Guy Worthington and Michael Wiley of BEST ENVIRONMENTAL INC.

Observing Personnel: No representatives from the Bay Area Air Quality Management District were present to witness the test on September 15, 1992.

Process Description: The natural gas fired turbine and steam turbine are used to supply power and steam to the Agnews Developmental Center. Exhaust from the gas fired turbine enters the boiler at approximately 1000°F, where steam is produced to drive a second power generating turbine.

Test Program: Triplicate 30 minute tests were performed for formaldehyde and acetaldehyde emissions. Two tests were conducted to determine the stack gas moisture and volumetric flowrate. A single integrated bag sample was collected for oxygen and carbon dioxide measurement and for molecular weight calculations. The Cogen was operated at the following conditions:

Gas Turbine 23.33 MW during test.

Steam Turbine 7.27 MW during test.

Natural gas consumption rate 11,400 lbs/hr

Sampling and Analysis Methods: The following California Air Resources Board (CARB) sampling and analytical methods were used:

CARB Method 430

Formaldehyde and Acetaldehyde

CARB Method 1,2,3,4

Volumetric Flowrate, Moisture, Molecular Weight

Instrumentation: The following emission analyzers were used:

O₂/CO₂

Fyrite wet chemical analyzer

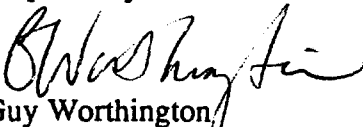
Test Results: Emission results are contained in Table 1. Formaldehyde was only detected in Test #1, and the average value is based upon including the detection limit for Test #2 and #3. Acetaldehyde was detected in Tests #1 and #2. The average includes the detection limit of Test #3. The average values of the stack gas moisture and flowrate tests were used to calculate the emission rates. The average emissions were as follows:

Formaldehyde	22.5 gm/hr
Acetaldehyde	26.2 gm/hr

Stack gas volumetric flowrate and moisture calculations, field data sheets, calculations, QAQC data, laboratory results and sample custody records are appended to this report.

If you have any questions regarding this report, or if BEST ENVIRONMENTAL can be of any further assistance, please call.

Prepared by


Guy Worthington
Project Manager

Reviewed by


Regan Best
Manager

RECEIVED OCT 0 6 1992

CALPINE

**Source Test Report
Agnews Cogeneration Facility
Test Date: September 15, 1992**

TABLE 1

Calpine - Agnews
Formaldehyde and Acetaldehyde Emission Results
CARB METHOD 430

Plant: Agnews

Source: Nat. Gas Cogen

Operating Condition: Gas Turbine @23.3MW, Steam Turbine @ 7.27MW

TEST #	1	2	3	AVERAGE*
Date	9/15/92	9/15/92	9/15/92	
Time	1254-1324	1339-1409	1422-1452	
Stack Gas Flowrate, (sdcfm)	127,143	127,143	127,143	127,143
Oxygen, %	14.5	14.5	14.5	14.5
Carbon Dioxide, %	3.6	3.6	3.6	3.6
Moisture Content, %	9.9	9.9	9.9	9.9
Sample Volume, (dscf)	0.478	0.465	0.453	0.465
Sample Volume, (dscm)	0.014	0.013	0.013	0.013
Formaldehyde, ug/sample	0.88	<0.50	<0.50	0.6
Formaldehyde, ug/dscm	65.0	<38.0	<39.0	47.3
Formaldehyde, ppb	52.3	<30.5	<31.4	38.1
Formaldehyde, gm/hr	31.0	<18.1	<18.6	22.5
Acetaldehyde, ug/sample	1.19	0.50	<0.50	0.7
Acetaldehyde, ug/dscm	87.9	38.0	<39.0	55.0
Acetaldehyde, ppb	48.1	20.8	<21.3	30.1
Acetaldehyde, gm/hr	41.9	18.1	<18.6	26.2

WHERE,

Formaldehyde Molecular Weight. = 30.0

Acetaldehyde Molecular Wt. = 44.1

sdcfm = Standard Dry Cubic Feet per Minute

dscf = Dry Standard Cubic Feet

ppb = Parts per Billion

M.W. = Molecular Weight

ug/dscm = Micrograms per Dry Standard Cubic Meter

gm/hr = Grams per Hour Emission Rate

CALCULATIONS,

gm/hr = sdcfm*60*(ug/sample)/(dscf*453600)

ppb = (ug/dscm)*(24.134/MW)

APPENDICES

CALCULATIONS

**BEST ENVIRONMENTAL
ALDEHYDE SAMPLING DATA CALCULATIONS
CARB METHOD 430**

Plant: Calpine - Agnews

Source: Cogen

TEST #	1	2	3
Date	9/15/92	9/15/92	9/15/92
Time	1254-1324	1339-1409	1422-1452
Meter Volume (Vm), ft ³	0.474	0.454	0.438
Meter Volume (liters)	13.42	12.86	12.40
Sample Rate (Lpm)	0.447	0.429	0.413
Meter Factor, (Yd)	1.0763	1.0763	1.0763
Barometric Pressure (Pb), "Hg	29.80	29.80	29.80
Meter Pressure (dH), "H ₂ O	0.1	0.1	0.1
Meter Temperature (tm), °F	104.1	94.80	89.40
Temperature Std (tstd), °F	70	70	70
Stack Gas Moisture, %	9.9	9.9	9.9
Sample Volume Std. (Vmstd), ft ³	0.478	0.465	0.453

WHERE,

$$T_{std} = t_{std} + 460^{\circ}R$$

$$P_m = P_b + (dH/13.6)$$

$$T_m = t_m + 460^{\circ}R$$

CALCULATIONS,

$$Vmstd = (Vm * Yd * Tstd * Pm) / (Tm * 29.92)$$

BEST ENVIRONMENTAL STACK MOISTURE DETERMINATION

Calpine - Agnews
Cogen

Date: 9/15/92
Time: 1230-1300

1. Uncorrected Meter Volume (Vm)	30.04	ft ³
2. Meter Factor (Yd)	0.9710	
3. Barometric Pressure (Pb)	29.80	"Hg
4. Meter Pressure (^H)	0.1	"H ₂ O
5. Meter Temperature (tm)	81.6	°F
6. Std. Temperature (tstd)	70.0	°F
7. Impinger H ₂ O Gain (VwH ₂ O)	40.0	ml
8. Silica Gel Wt. Gain (Vwsg)	23.0	gm
9. Moisture Vapor (Vw std)	2.98	ft ³
 Std. Meter Volume (Vm std)	 28.437	 ft ³
Percent of H ₂ O in Stack (% H ₂ O)	9.5	%

WHERE,

ft³ = Cubic Feet
Hg = Mercury
°F = Degrees Fahrenheit
ml = milliliters
gm = grams
% = Percent

CALCULATIONS,

Moisture Vapor = $0.00267 \times (VwH_2O + Vwsg) \times (460 + tstd) / 29.92$
Std. Meter Vol. = $Vm \times Yd \times (tstd + 460) \times (Pb + ^H/13.6) / (tm - 460) \times 29.92$
Stack Moisture = Moisture Vapor / Moisture Vapor + Vm std

**BEST ENVIRONMENTAL
STACK MOISTURE DETERMINATION**

Calpine - Agnews

Cogen

Date: 9/15/92

Time: 1340-1410

1. Uncorrected Meter Volume (Vm)	17.857	ft ³
2. Meter Factor (Yd)	0.9710	
3. Barometric Pressure (Pb)	29.80	"Hg
4. Meter Pressure (^H)	0.1	"H ₂ O
5. Meter Temperature (tm)	77.1	°F
6. Std. Temperature (tstd)	70.0	°F
7. Impinger H ₂ O Gain (VwH ₂ O)	34.0	ml
8. Silica Gel Wt. Gain (Vwsg)	7.0	gm
9. Moisture Vapor (Vw std)	1.94	ft ³
Std. Meter Volume (Vm std)	17.046	ft ³
Percent of H ₂ O in Stack (% H ₂ O)	10.2	%

WHERE,

ft³ = Cubic Feet
Hg = Mercury
°F = Degrees Fahrenheit
ml = milliliters
gm = grams
% = Percent

CALCULATIONS,

Moisture Vapor = $0.00267 \times (VwH_2O + Vwsg) \times (460 + tstd) / 29.92$
Std. Meter Vol. = $Vm \times Yd \times (tstd + 460) \times (Pb + ^H/13.6) / (tm + 460) \times 29.92$
Stack Moisture = Moisture Vapor / Moisture Vapor + Vm std

BEST ENVIRONMENTAL STACK VOLUMETRIC FLOW RATE DETERMINATION

Calpine - Agnews
Cogen

Date: 9/15/92
Time: 1356

1. Avg. (SQRT ΔP)	1.017 H ² O
2. Pitot Coefficient (Cp)	0.84
3. Temperature of Stack (ts)	323.0 °F
4. Barometric Pressure (Pb)	29.80 "Hg
5. Static Pressure (Pstatic)	-0.7 H ² O
6. Stack Pressure (Ps)	29.75 "Hg
7. Percent of H ² O in Stack (%)	9.9 %
8. Molecular Weight of Stack Gas (MWs)	28.06 lb/lb-mole
A. Percent O ₂	14.5 %
B. Percent CO ₂	3.6 %
C. Percent CO	0.0 %
9. Area of Stack ft ² (As)	49.224 ft ²

STACK GAS VELOCITY , Actual (Vs)	70.7 ft/sec
STACK GAS VOL. FLOWRATE, (Qactual)	208,915 ACFM
STACK GAS VOL. FLOWRATE (Qstd)	126,273 SDCFM

WHERE, Vs = Velocity of the stack gas, actual (ft/sec)
 Qstd = Volumetric flowrate at standard conditions
 MWs = Molecular Wt. Stack Gas, wet basis
 MWd = Molecular Wt. Stack Gas, dry basis
 Ps = Stack pressure
 ΔP = Differential pressure measured by the pitot
 ACFM = Actual Cubic Feet Per Minute
 SDCFM = Standard Dry Cubic Feet Per Minute
 Bws = %H₂O / 100

CALCULATIONS,

$$\begin{aligned}
 MWs &= (MWd) \times (1-Bws) + 18 (Bws) \\
 MWd &= .44 (\%CO_2) + .32 (\%O_2) + .28 (\%CO + \%N_2) \\
 Ps &= Pb + (Pstatic / 13.6) \\
 Vs &= 85.49 \times Cp \times \sqrt{\Delta P} \times \sqrt{(ts + 460) / (Ps \times MWs)} \\
 Q_{actual} &= 60 \times Vs \times As \\
 Q_{std} &= 60 \times Vs \times As \times 528 / (ts + 460) \times Ps / 29.92 \times (1-Bws)
 \end{aligned}$$

BEST ENVIRONMENTAL STACK VOLUMETRIC FLOW RATE DETERMINATION

Calpine - Agnews
Cogen

Date: 9/15/92
Time: 1433

1. Avg. (SQRT ^P)	1.031 H ² O
2. Pitot Coefficient (Cp)	0.84
3. Temperature of Stack (ts)	323.0 °F
4. Barometric Pressure (Pb)	29.80 "Hg
5. Static Pressure (Pstatic)	-0.7 H ² O
6. Stack Pressure (Ps)	29.75 "Hg
7. Percent of H ² O in Stack (%)	9.9 %
8. Molecular Weight of Stack Gas (MWs)	28.06 lb/lb-mole
A. Percent O ₂	14.5 %
B. Percent CO ₂	3.6 %
C. Percent CO	0.0 %
9. Area of Stack ft ² (As)	49.224 ft ²

STACK GAS VELOCITY , Actual (Vs)	71.7 ft/sec
STACK GAS VOL. FLOWRATE, (Qactual)	211,791 ACFM
STACK GAS VOL. FLOWRATE (Qstd)	128,012 SDCFM

WHERE, Vs = Velocity of the stack gas, actual (ft/sec)
 Qstd = Volumetric flowrate at standard conditions
 MWs = Molecular Wt. Stack Gas, wet basis
 MWd = Molecular Wt. Stack Gas, dry basis
 Ps = Stack pressure
 ^ P = Differential pressure measured by the pitot
 ACFM = Actual Cubic Feet Per Minute
 SDCFM = Standard Dry Cubic Feet Per Minute
 Bws = %H₂O / 100

CALCULATIONS,

$$\begin{aligned}
 MWs &= (MWd) \times (1-Bws) + 18 (Bws) \\
 MWd &= .44 (\%CO_2) + .32 (\%O_2) + .28 (\%CO + \%N_2) \\
 Ps &= Pb + (Pstatic / 13.6) \\
 Vs &= 85.49 \times Cp \times \sqrt{^P} \times \sqrt{(ts + 460) / (Ps \times MWs)} \\
 Qactual &= 60 \times Vs \times As \\
 Qstd &= 60 \times Vs \times As \times 528 / (ts + 460) \times Ps / 29.92 \times (1-Bws)
 \end{aligned}$$

FIELD DATA SHEETS

BEST ENVIRONMENTAL
Stack Gas Volumetric Flowrate Determination

Client: <u>ALPINE</u>					Location: <u>AGNEWS COGEN (BOILER-TURBINE)</u>				
Date: <u>9-15-92</u> Time: <u>1356</u>					Run#: <u>1</u>				
Pitot Factor (Cp): <u>0.84</u> ID# <u>22</u>					Operators: <u>GW, MW</u>				
Assumed %O2: <u>14.5</u> Actual <u>14.5</u>					Barometric (Pb): <u>29.80</u>				
Assumed %CO2: <u>3.6</u> Actual <u>?3.6</u>					Static Pressure (Pstatic): <u>-0.70</u>				
Assumed %CO: <u> </u> Actual <u> </u>					Stack Diameter, in: <u>7'11" (95")</u>				
Assumed %H2O: <u>5.5</u> Actual <u>9.85%</u>					Stack Area, ft² (As): <u>49.224</u>				

Port ID & Point#	Point Location, Inches	Delta P, ("P)	Stack Temp °F, (ts)	SORT "P	CALCULATIONS
<u>South 1</u>	<u>2.0</u>	<u>1.4</u>	<u>323</u>	<u>1.183</u>	<u>Stack Gas Velocity, actual feet per sec (Vs)</u> $V_s = 85.49 \cdot C_p \cdot (SORT \cdot P)_{avg} \cdot SORT / [(ts + 460) / P_s \cdot MW_s]$ Vs =
<u>2</u>	<u>6.4</u>	<u>1.0</u>	<u>323</u>	<u>1.183</u>	
<u>3</u>	<u>11.2</u>	<u>1.00</u>	<u>323</u>	<u>1.000</u>	
<u>4</u>	<u>16.8</u>	<u>0.95</u>	<u>323</u>	<u>0.975</u>	<u>Molecular Weight of Stack Gas, g/g.mole (MWs)</u> $MW_s = MW_d \cdot (1 - B_{wo}) + 18(B_{wo})$ MWs =
<u>5</u>	<u>23.8</u>	<u>0.86</u>	<u>323</u>	<u>0.927</u>	
<u>6</u>	<u>33.6</u>	<u>0.76</u>	<u>323</u>	<u>0.872</u>	
<u>7</u>	<u>61.2</u>	<u>0.94</u>	<u>323</u>	<u>0.970</u>	<u>Molecular Weight of Dry Gas, g/g.mole (MWd)</u> $MW_d = 0.44(\%CO_2) + 0.32(\%O_2) + 0.28(\%CO + N_2)$ MWd =
<u>8</u>	<u>71.3</u>	<u>1.00</u>	<u>323</u>	<u>1.080</u>	
<u>9</u>	<u>78.2</u>	<u>1.2</u>	<u>323</u>	<u>1.095</u>	
<u>10</u>	<u>83.8</u>	<u>1.4</u>	<u>323</u>	<u>1.183</u>	<u>Stack Gas Volumetric Flow Rate, standard dry cubic feet/min (SDCFM)</u> $SDCFM = 60(1 - B_{wo}) \cdot V_s \cdot A_s \cdot 528 / [(ts + 460) \cdot P_s / 29.92]$ SDCFM =
<u>11</u>	<u>88.6</u>	<u>0.95</u>	<u>323</u>	<u>0.975</u>	
<u>12</u>	<u>93.0</u>	<u>0.70</u>	<u>323</u>	<u>0.837</u>	
					WHERE: <u>Stack Pressure, "Hg (Ps)</u> $P_s = P_b + (P_{static}/13.6)$ <u>Water Vapor Fraction, (Bwo)</u> $B_{wo} = \%H_2O/100$ <u>Stack Area, ft² (As)</u> $A_s = (Diameter/24)² \cdot 3.1416$ Comments: <u>West port not accessible due to obstruction in line with of pitot, about 5' from port.</u>
AVG					

BEST ENVIRONMENTAL
Stack Gas Volumetric Flowrate Determination

Client: <u>CALPINE - AGNEWS</u>					Location: <u>CODEN</u>				
Date: <u>9-15-92</u> Time: <u>1433</u>					Run#: <u>2</u>				
Pitot Factor (Cp): <u>0.84</u>					Operators: <u>GL, MW</u>				
Assumed %O2: Actual <u>14.5</u>					Barometric (Pb): <u>29.80</u>				
Assumed %CO2: Actual <u>3.6</u>					Static Pressure (Pstatic): <u>-0.80</u>				
Assumed %CO: Actual					Stack Diameter, in: <u>95"</u>				
Assumed %H2O: Actual <u>9.85%</u>					Stack Area, ft² (As): <u>49.224</u>				
Port ID & Point#	Point Location, Inches	Delta P, (P)	Stack Temp °F. (ts)	SQRT P	CALCULATIONS				
1		1.4	323	1.183	<u>Stack Gas Velocity, actual feet per sec (Vs)</u> $V_s = 85.49 \cdot C_p \cdot (\text{SQRT } P_{\text{avg}} \cdot \text{SQRT}[(t_s + 460)/P_s \cdot M W_s])$ Vs =				
2		1.3	324	1.140					
3		1.1	324	1.049					
4		0.93	324	0.964	<u>Molecular Weight of Stack Gas, g/g.mole (MWs)</u> $M W_s = M W_d \cdot (1 - B w_o) + 18(B w_o)$ MWs =				
5		0.85	324	0.922					
6		0.88	324	0.938					
7		0.90	324	0.949	<u>Molecular Weight of Dry Gas, g/g.mole (MWd)</u> $M W_d = 0.44(\%CO_2) + 0.32(\%O_2) + 0.28(\%CO + N_2)$ MWd =				
8		0.98	324	0.990					
9		1.10	324	1.049					
10		1.30	324	1.140	<u>Stack Gas Volumetric Flow Rate, standard dry cubic feet/min (SDCFM)</u> $SDCFM = 60(1 - B w_o) \cdot V_s \cdot A_s \cdot 528 / (t_s + 460) \cdot P_s / 29.92$ SDCFM =				
11		1.20	324	1.095					
12		0.90	324	0.949					
					WHERE;				
					<u>Stack Pressure, "Hg (Ps)</u> $P_s = P_b + (P_{\text{static}}/13.6)$				
					<u>Water Vapor Fraction, (Bwo)</u> $B w_o = \%H_2O/100$				
					<u>Stack Area, ft² (As)</u> $A_s = (\text{Diameter}/24)^2 \cdot 3.1416$				
					Comments:				
AVG									

outer.

BEST ENVIRONMENTAL Particulate Field Data Sheet

Run # 1,2 Method # 4

Plant CALPINE - AGNEWS
 Date 9-15-92
 Location BOILER/TURBINE
 Port Dia. _____
 Stack I.D. 95"
 Stack Area _____ ft²
 Personnel GW, MW

Orif. 2.385 XH₂O Assum. 5.5
 Meter Yd 0.9710 Pitot Cp 0.84
 PBar. 29.80 Noz. Diam. _____
 Stat Press _____ Noz. I.D. _____
 XCO₂ Assum 14.5 Meter # 8811
 XCO₂ Assum 3.6 Probe # _____
 Pre leak ck <0.01 cfm 24 "Hg Post leak ck <0.01 cfm 15 "Hg
 <0.01 14 <0.01 4

Filter # _____ F.H. Wt. (mg) _____
 Pitot # E' Z.H. Wt. (mg) _____
 Net Imp Vol 40 ml. Gel Wt. (mg) _____
 Tot Imp Vol _____ XCO₂ Actual _____
 Sample Time 30 XCO₂ Actual _____
 Sqrt ΔP Ave _____ Tot. Moisture _____
 Std Vm _____

Sample Point	Clock Time	Vel. ΔP	K.R. cfm	Orif. ΔH	Gas Meter Volume ft ²	Gas Meter		Temperatures F				Pump Vac.	Comments
						In	Out	Stack	Imp.	Filter	Probe		
1 START	1230		~0.5	0.1	274.820	79	78		468			14	
2	1235				277.3	81	82					15	
3	1240				283.3	81	82					14	
4	1245				288.8	82	83					13	
5	1250				293.5	82	83					13	
6	1255				299.1	83	83					13	
7 STOP	1300				304.860								
8	1305												
9					<30.040> <8.0>								
10													
11 START	1340		~0.5	0.1	305.250	77	78		468			2	
12	1345				306.4	76	78					2	
13	1350				311.7	76	78					2	
14	1355				314.0	76	78					2	
15	1400				317.4	76	78					2	
16	1405				320.2	76	78					2	
17 STOP	1410				323.107								
18													
19					17.857	<77.1>							
20													
21													
22													
23													
24													
25													
26													
27													
28 Average													

Notes:

	Run 1	Run 2
ml.	40	34
mg.	23	7
	<u>63</u>	<u>41</u>

As =
 Ave. Vs =
 Sample I.D. # =

Final Imp Vol =
 Initial Imp Vol =

FIGURE 4: (A) RECORDING AND REPORTING - SAMPLING RUN DATA RECORD

(Note: Only one sampling run per data sheet.)

Run #: 1 Project #: C-7 / Pilot
 Location: Outlet Source Name: Cogco
 Date Sampled: 9-15-92 Operator: MV
 Meter Yd 1.0763 Pbar 29.80

	Clock Time	Meter Rotameter Reading	Flow Rate, Q mL/min	Impinger Temp. °F	Stack Temp. °F	Meter Temp. °F	COMMENTS
0	12:54	145.499				100	out
1	5 min	145.592	0.030527			102	107
2	10 min	145.659	0.040362			103	107
3	15 min	145.745	0.050487			103	107
4	20 min	145.816	0.071040			102	106
5	25 min	145.884	0.080385			102	106
6	30 min	145.973	0.080504			101	106 Avg 104.1

$(.474) = 13.4 \text{ L Flow rate} = 0.447 \text{ L/min}$

Chain of Custody Record Numbers, Sample Id. Numbers, Tare Masses, and Final Masses

Suggested Codes:

I&V w/ id. # ≡ Impinger, Transport, & Extraction Vial (all)

IMP w/ id. # ≡ Impinger (only)

E&T w/ id. # ≡ Extraction and Transport Vial (both)

C.O.C. #	S. Id. #	m _{tare} (tare mass)	m _{final} (final mass)
	1A (R-1 Imp1)	31 g	
	1B (R-1 Imp2)	31 g	

FIGURE 4: (A) RECORDING AND REPORTING - SAMPLING RUN DATA RECORD

(Note: Only one sampling run per data sheet.)

Run #: 2 Project #: _____
 Location: atlet Source Name: Calpine Co-gen
 Date Sampled: 9-15-92 Operator: MW

	Clock Time	Meter Rotameter Reading	Flow Rate, Q mL/min	Impinger Temp. °F	Stack Temp. °F	COMMENTS
0	13:37	146.994	CF			Meter Temp 98 101
1	5 min	146.066	$\frac{.014}{.070}$			98 100
2	10 min	146.134	$\frac{.0136}{.068}$			96 100
3	15 min	146.224	$\frac{.0150}{.068}$			92 96
4	20 min	146.286	---			90 93
5	25 min	---	---			90 92
6	30 min	146.450	---			89 92 Avg 94.8

$$\langle .454 \rangle = 12.86 \text{ L Flow rate} = .429 \text{ L/min}$$

Chain of Custody Record Numbers, Sample Id. Numbers, Tare Masses, and Final Masses

Suggested Codes:

I&V w/ id. # $\equiv$ Impinger, Transport, & Extraction Vial (all)

IMP w/ id. # $\equiv$ Impinger (only)

E&T w/ id. # $\equiv$ Extraction and Transport Vial (both)

C.O.C. #	S. Id. #	m _{tare} (tare mass)	m _{final} (final mass)
	2A(R-2Imp1)	31	33
	2B(R-2Imp2)	30	30

FIGURE 4: (A) RECORDING AND REPORTING - SAMPLING RUN DATA RECORD

(Note: Only one sampling run per data sheet.)

Run #: 3 Project #: _____
 Location: Outlet Source Name: CalPine Cogeneration
 Date Sampled: 9-15-92 Operator: MW

	Clock Time	Meter Rotameter Reading	Flow Rate, Q mL/min	Impinger Temp. °F	Stack Temp. °F	Meter trap IN out COMMENTS
0	14:22	146.477	---	815		89 91
1	5 min	146.538	$\frac{0.0182}{0.041}$ 515			88 90
2	10 min	146.622	$\frac{0.0169}{0.041}$ 476			88 90
3	15 min	146.688	$\frac{0.0132}{0.036}$ 374			88 90
4	20 min	146.763	$\frac{0.0150}{0.035}$ 425			88 90
5	25 min	146.850	$\frac{0.0174}{0.037}$ 494			89 91
6	30 min	146.915	$\frac{0.065}{0.036}$ 368			88 91 Avg 89.4.

$$\langle 0.438 \rangle 12.4 \text{ L} = 0.413 \text{ L/min}$$

Chain of Custody Record Numbers, Sample Id. Numbers, Tare Masses, and Final Masses

Suggested Codes:

I&V w/ id. # $\equiv$ Impinger, Transport, & Extraction Vial (all)

IMP w/ id. # $\equiv$ Impinger (only)

E&T w/ id. # $\equiv$ Extraction and Transport Vial (both)

C.O.C. #	S. Id. #	m _{tare} (tare mass)	m _{final} (final mass)
	BA(R-IMP1)	30 gr	33 gr
	BB(R-IMP2)	31 gr	30 gr

LAB REPORTS

AIR TOXICS LTD.

Stationary Source Test Method - Formaldehyde

(CARB Method 430)

High Pressure Liquid Chromatography

Field Sample I.D.	Lab Sample I.D.	File Name	Sample Date	Analyzed For	Total Volume (mL)	Dilution Factor	MDL (uG)	Amount (uG)
Run-1 UMP 1	9209082-01A	4091802	9/15/92	Formaldehyde	12.2	1.0	0.50	0.88
				Acetaldehyde			0.50	0.50
Run-1 UMP 1 Duplicate	9209082-01AA	4091803	9/15/92	Formaldehyde	12.2	1.0	0.50	0.84
				Acetaldehyde			0.50	0.50
R1IMP2	9209082-01B	4091804	9/15/92	Formaldehyde	9.0	1.0	0.50	Not Detected
				Acetaldehyde			0.50	0.69
R2IMP1	9209082-02A	4091806	9/15/92	Formaldehyde	12.0	1.0	0.50	Not Detected
				Acetaldehyde			0.50	Not Detected
R2IMP2	9209082-02B	4091807	9/15/92	Formaldehyde	9.2	1.0	0.50	Not Detected
				Acetaldehyde			0.50	0.50
R3IMP1	9209082-03A	4091808	9/15/92	Formaldehyde	12.6	1.0	0.50	Not Detected
				Acetaldehyde			0.50	Not Detected
R3IMP2	9209082-03B	4091809	9/15/92	Formaldehyde	9.0	1.0	0.50	Not Detected
				Acetaldehyde			0.50	Not Detected
R4IMP1	9209082-04A	4091810	9/15/92	Formaldehyde	12.8	1.0	0.50	Not Detected
				Acetaldehyde			0.50	Not Detected
R4IMP2	9209082-04B	4091811	9/15/92	Formaldehyde	7.4	1.0	0.50	Not Detected
				Acetaldehyde			0.50	Not Detected
Trip Blank	9209082-05A	4091814	9/15/92	Formaldehyde	10.0	1.0	0.50	Not Detected
				Acetaldehyde			0.50	Not Detected
Lab Blank	9209082-07A	4091816	NA	Formaldehyde	10.0	1.0	0.50	Not Detected
				Acetaldehyde			0.50	Not Detected
Spiked Samples								% Recovery
R1IMP2 Matrix Spike	9209082-01B-MS	4091805	9/15/92	Formaldehyde	9.0	1.0	0.50	104
				Acetaldehyde			0.50	98
Trip Spike	9209082-06A	4091815	9/15/92	Formaldehyde	11.0	1.0	0.50	87
				Acetaldehyde			0.50	89
Lab Spike	9209082-08A	4091817	NA	Formaldehyde	11.0	1.0	0.50	101
				Acetaldehyde			0.50	96

Extraction Date: 9/17/92

Analysis Date: 9/18/92

COMMENTS: NA=Not Applicable

BEST ENVIRONMENTAL

18800 Foxhill Blvd

San Leandro, CA 94578

Phone (510) 278-4011 Fax (510) 278-4018

P.O. # = GW91592

CHAIN-OF-CUSTODY RECORD AND ANALYSIS REQUEST

Page 1 of 1

CUSTODY RECORD

ANALYSIS REQUEST

Project Manager:

GUY WORTHINGTON

Lab Name

AIR TOXICS

Client:

CALPINE

location:

I attest that the proper field sampling procedures were used during the collection of these samples.

Sampler Name (Print):

MIKE WILBY

Field Sample ID	Volume	# CONTAINERS:	Matrix			Method Preserved								Sampling	
			WATER	AIR	OTHER	HCl	HNO ₃	H ₂ SO ₄	ICE	NONE	OTHER	DATE	TIME		
RUN-1 IMP1		1	X									9/15		CARB 429	(PAHs)
R-1 IMP2		1	X											CARB 428	(Dioxins)
R-2 IMP1		1	X											CARB 410A	410B (Benzene)
R-2 IMP2		1	X											CARB 430	(Aldehydes)
R-3 IMP1		1	X											CARB 421	(HCl)
R-3 IMP2		1	X											CARB 425	(CFCs)
R-4 IMP1		1	X											CARB 422	(Hap. Ops)
R-4 IMP2		1	X											CARB 106	(vinyl chloride)
														EPA 600	(Elut metals, chlorides)
														CARB 426	(Cyanide)
														CARB 423	(Arsenic)
														CARB 427	(Asbestos)
														CARB 436	

SPECIAL HANDLING

24 HOURS ☐

EXPEDITED 48 Hours ☐

NTAT ☒

OTHER ☐ (#) BUSINESS DAYS

Return tedlars _____

Return cooler _____

Return bottles _____

SPECIAL DETECTION LIMITS (Specify)

SPECIAL REPORTING REQUIREMENTS

Air samples- total qty. to be reported

REMARKS:

FORMAL SETBACK ONLY.

Received by:	Time	Date	Relinquished by Sampler:
Express H. Owners		9/16/92	GW
Received by:	Time	Date	Relinquished by:
Received by Laboratory:	Time	Date	Relinquished by:
Express H. Owners Way bill # I1620215		9/17/92 09:35	Allyson Mungata

EQUIPMENT CALIBRATION RECORDS

METER BOX FULL TEST CALIBRATION

DATE: 6/10/92
 OPERATOR: MW

METER BOX Yd: 1.0763
 METER BOX ΔH@: —

ΔH@: —
 METER ~~Wd~~: 033501
 BAROMETRIC PRESSURE (Pb): 29.91
10

Q	h ₁	2	3	Standard Meter Gas Volume (ft ³)			Meter Box Gas Volume (ft ³)			Standard Meter Temperature			Meter Box Temperature			Time (Min.)	ΔH@	Yd
				Initial	Final	4 (Vd/s) Net	Initial	Final	5 (Vd) Net	In	Out	6 Tds Avg	In	Out	7 Td Avg	8		
.035			1.0000			.5297	106.596	107.093	.498			73.4	76.2	75.6	76.1	14.99		1.0689
.035			1.0000			.5297	107.093	107.591	.497			72.2	76.1	76.0	76.1	14.92		1.0660
.024			1.000			.5297	108.377	108.875	.498			72.6			76	21.81		1.070
.024			1.000			.5297	108.875	109.372	.497			72.6			76	21.95		1.072
.014			1.0000			.4237	109.474	109.868	.394			73.1			76	30.85		1.0812
.013			1.0000			.4237	109.868	110.255	.387			73.5			76	31.37		1.0899

- Q = Flow Rate (cfm)
 ΔH - Orifice Pressure Differential (in. H₂O)
 ΔP - Inlet Pressure Differential Standard Meter (in. H₂O)
 Yds - Standard Meter Correction Factor (Unitless)
 Yd - Meter Box Correction Factor (Unitless)
 ΔH@ - Orifice Pressure Differential that gives 0.75 cfm of air at 70°F and 29.92" Hg (in. H₂O)

$$Yd = (Yds) \left(\frac{Vds}{Vd} \right) \left(\frac{Td + 460}{Tds + 460} \right) \left(\frac{Pb + \Delta P / 13.6}{Pb + \Delta H / 13.6} \right)$$

$$\Delta H@ = \frac{0.0317 \Delta H}{Pb (Td + 460)} \left[\frac{(Tds + 460) \theta}{Vds \cdot Yds} \right]^2$$

$$Q = \frac{17.64 \cdot Vds \cdot Pb}{(Td + 460)}$$

Date: 3-9-92

Pitot Number: 22

TYPE S PITOT TUBE INSPECTION DATA

Pitot tube assembly level? yes ✓ no

Pitot tube openings damaged? yes (explain below) ✓ no

$\alpha_1 = \underline{0^\circ}$ ($< 10^\circ$), $\alpha_2 = \underline{0.5^\circ}$ ($< 10^\circ$), $\beta_1 = \underline{1.5^\circ}$ ($< 5^\circ$)

$\beta_2 = \underline{1.5^\circ}$ ($< 5^\circ$)

$Y = \underline{1.5^\circ}$, $\theta = \underline{0.75^\circ}$, $A = \frac{1.082}{1.167} \text{ cm (in.)}$

$Z = A \sin Y = \frac{0.03}{0.31} \text{ cm (in.)}; < 0.32 \text{ cm } (< 1/8 \text{ in.}),$

$W = A \sin \theta = \underline{0.01} \text{ cm (in.)}; < 0.08 \text{ cm } (< 1/32 \text{ in.})$

$P_a = \underline{0.375} \text{ cm (in.)}$ $P_b = \underline{0.375} \text{ cm (in.)}$

$D_t = \underline{1.082} \text{ cm (in.)}$ $\frac{\bar{P}}{D_t} = \frac{1.44}{P_a = P_b = P} (\geq 1.05 \text{ and } \leq 1.50)$

COMMENTS: 8' S-Type Pitot Tube

Calibration required? yes ✓ no

Calibrated by: MW