



State of New Jersey
DEPARTMENT OF ENVIRONMENTAL PROTECTION
DIVISION OF ENVIRONMENTAL QUALITY
Bureau of Technical Services
CN 411
Trenton, N.J. 08625-0411
(609) 530-4041

March 11, 1991

MEMORANDUM

TO: Chief, Bureau of Enforcement Operations

THROUGH: Edward Choromanski 

FROM: Michael Pratt 

SUBJECT: Algonquin Gas Transmission Company
APC Plant ID No. 25157
NJ Stack Nos. 001 and 002
P/CT Nos. 75952 and 75953
Log Nos. 85-0654 and 85-0655

Emission tests were conducted at the above referenced facility on two gas turbines (GT-1 and GT-2 Solar Turbines International).

The purpose of these tests was to determine:

- 1) CO, THC (as C_3H_8) and NO_x (as NO) emissions and then to compare the emission results for each air contaminant to the P/CT Nos: 75952 and 75953 allowables.
- 2) Compliance with USEPA, NSPS 40 CFR, Part 60, Subpart GG (Stationary Gas turbines).

Richelle Burkeen reviewed the submitted test report. Her review indicated the following:

- 1) GT-1 "Solar Turbine International" was operating during stack testing at 65% to 104% of its maximum capacity.
- 2) GT-2 "Solar Turbine International" was operating during stack testing at 102 to 105% of its maximum capacity.
- 3) Both "Solar" gas turbines emissions were in compliance with USEPA NSPS 40 CFR, Part 60, Subpart GG (Stationary Gas Turbines).



- 4) CO, THC (as C₃H₈), and NO_x (as NO) emissions were within P/CT Nos. 75952 and 75953 allowables.

CONCLUSIONS:

- 1) Compliance with P/CT No. 75952 and 75953.
- 2) Compliance with USEPA, NSPS 40 CFR, Part 60, Subpart GG.

RECOMMENDATION:

P/CT Nos. 75952 and 75953 can be changed to permanent status pending approval by NRO.

c: Milton Polakovic
Lou Mikolajczyk
Michael Papp
Richelle Burkeen



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February 15, 1991

MEMORANDUM

TO: Michael Pratt

FROM: Richelle Burkeen *RSB*

SUBJECT: Algonquin Gas Transmission Company
Hanover, New Jersey
APC ID No. 25153
NJ Stack No. 001 and 002
P/CT No. 075952 and 075953

The above referenced facility was tested on November 13 and 14, 1990 for nitrogen oxide, carbon monoxide, and total hydrocarbon emissions. Gas turbines one and two were the sources of these emissions. TRC Environmental Consultants, Inc. of East Hartford, Connecticut conducted the emission tests and the results are as follows.

STACK 001

	Run 1	Run 2	Run 3	Allowable
Carbon Monoxide				
ppm	8.5	8.7	10.7	
ppm @7% O ₂	29.8	42.0	39.4	
lb/hr	1.39	1.27	1.58	7.9
Total Hydrocarbons (as C₃H₈)				
ppm	<0.1	2.5	<0.1	
ppm @7% O ₂	<0.35	12.1	<0.37	
lb/hr	<0.03	0.64	<0.02	2.3
Nitrogen Oxide (as NO)				
ppm	78.9	55.1	85.6	
ppm @15% O ₂	119.0	116.1	136.5	160*
ppm @15% O ₂ & ISO	112.6	114.9	126.9	
lb/hr	13.8	8.64	13.6	17.4



STACK 002

	Run 1	Run 2	Run 3	Allowable
Carbon Monoxide				
ppm	8.2	9.7	9.2	
ppm @7% O ₂	33.8	34.8	33.0	
lb/hr	1.44	1.70	1.61	7.9
Total Hydrocarbons (as C₃H₈)				
ppm	<0.1	<0.1	<0.1	
ppm @7% O ₂	<0.41	<0.36	<0.36	
lb/hr	<0.023	<0.025	<0.025	2.3
Nitrogen Oxide (as NO)				
ppm	67.3	76.8	76.3	
ppm @15% O ₂	120.3	119.2	118.5	160*
ppm @15% O ₂ & ISO	115.7	112.9	109.9	
lb/hr	10.5	13.1	13.0	17.4

"<" denotes emissions below detection limit

* - Allowable as per NSPS Subpart GG. Standards for Stationary Gas Turbines.

Technical Services calculations of the raw data supplied indicate substantially the same results. The results indicate that mass emission rates for carbon monoxide, total hydrocarbons, and nitrogen oxide are within the allowables as per P/CT No. 075952 and 075953. Nitrogen oxide emissions also are in compliance with subpart GG, for mass concentrations at 15% O₂.

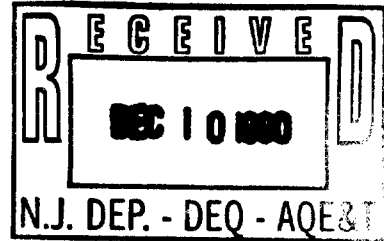
The operating conditions of the turbines is as follows:

	Turbine 1 Run 1	Run 2	Run 3
Fuel Flow (MMBTU/HR)	40	32	31
Combustor Inlet Pressure (PSIG)	122	93	122
Operating Load (HP)	3980	2522	3873

TURBINE 2

	RUN 1	RUN 2	RUN 3
Fuel Flow (MMBTU/HR)	41	41	41
Combustor Inlet Pressure (PSIG)	124	123	122
Operating Load (HP)	4011	3940	3918

The turbine engines are two 3830 hp engines. Therefore, turbine one operated at 65-104% of maximum capacity and turbine two operated at 102-105% of maximum capacity.



AIR POLLUTANT COMPLIANCE
TEST REPORT
STATIONARY GAS TURBINES 001 AND 002
ALGONQUIN GAS TRANSMISSION COMPANY
HANOVER COMPRESSOR STATION
HANOVER, NEW JERSEY

Prepared By:

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TRC Project No. 7638-E31

November, 1990

TRC

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A **TRC** Company

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1.0 INTRODUCTION

TRC Environmental Consultants, Inc. of East Hartford, Connecticut was retained by Algonquin Gas Transmission Company of Boston, Massachusetts, to perform a compliance emission test program at their Hanover, New Jersey facility. This test program was performed for the renewal of Algonquin's permits to operate their two gas turbines located at the Hanover compressor station. The parameters measured for compliance were nitrogen oxides, carbon monoxide, and total hydrocarbons. Three tests were run on each turbine.

The test program began with testing on Turbine No. 1 on November 13, 1990 with the turbine running at or near 100% of capacity. After the second test, there was no demand for natural gas and the compressor's bypass system could not facilitate running at 100%. Therefore, only two tests were completed that day. The third test for the Turbine No. 1 was completed after three tests were performed on Turbine No. 2 on November 14, 1990. The test program was performed by John DeGirolamo, Scott Neumann and Andrew Bykowski of TRC. Testing was coordinated by Nelson Strauch of Algonquin. Present to observe the test program were Howard Blostein and Frank Papp from the New Jersey Department of Environmental Protection (NJDEP).

Section 2.0 of this report presents the summary and discussion of results. The process description is given in Section 3.0 and the sampling and analytical methods are explained in Section 4.0. Section 5.0 outlines TRC's quality assurance program.

2.0 SUMMARY AND DISCUSSION OF RESULTS

The results are reported in two major sections. The first presents the sample and stack conditions and the New Jersey Air Test Method 3 pollutant emissions. The second section presents the ambient weather conditions and the results of the oxides of nitrogen testing. All supporting calculations can be found in Appendix E.

2.1 Gaseous Pollutant Emissions

The NJDEP required that the measurement of total hydrocarbons (THC) and carbon monoxide (CO) be performed in this sampling program. These pollutants were measured from both turbine's exhausts, the results of which are summarized in Table 2-1. The results for Turbine No. 1 showed an average concentration 9.3 ppm with an average emission rate of 1.41 lb/hr for CO. The total hydrocarbon concentration averaged 0.93 ppm as propane with an average emission rate of 0.23 lb/hr. Only one of the three tests on this turbine yielded a detectable result. The results for Turbine No. 2 varied little from turbine No. 1 and are presently in Table 2-2. The CO concentration averaged 9.0 ppm and the emission rate averaged 1.40 lb/hr. Total hydrocarbons as propane were not detected during the tests on Turbine No. 2.

2.2 Oxides of Nitrogen Emissions

Nitrogen Oxide (NOx) emissions were measured as Nitric Oxide (NO). Before entering the detector, all NOx was converted into NO. The NOx results are reported in uncorrected ppm, ppm corrected to 15% oxygen, and corrected to 15% oxygen at ISO conditions. The emission rates are presented in lbs/hr. Tables 2-3 and 2-4 summarized these results. The average concentration for Turbine No. 1 was

73.2 ppm uncorrected, 126.1 ppm corrected to 15% oxygen, and 120.3 corrected to 15% oxygen at ISO conditions. The average emission rate was 12.0 lbs/hr. Turbine No. 2 showed average concentrations of 73.5 ppm uncorrected, 119.3 ppm corrected to 15% oxygen, and 112.5 ppm corrected to 15% oxygen at ISO conditions. The average emission rate was 12.2 lbs/hr.

TABLE 2-1

SUMMARY OF MEASURED AIR POLLUTANTS
TURBINE NO. 1
ALGONQUIN GAS TRANSMISSION COMPANY
HANOVER, NEW JERSEY

Test Date Time	T-1 11/13/90 1130-1246	T-2 11/13/90 1400-1528	T-3 11/13/90 1540-1658	Average
<u>Stack Conditions</u>				
Flowrate (DSCFM)	37500	33600	33900	34800
Temperature (°F)	778	712	786	759
Moisture (%)	3.2	3.5	3.9	3.5
Oxygen (%)	17.0	18.1	17.2	17.4
<u>Pollutant Emissions</u>				
Concentration ^a				
Carbon Monoxide (ppm)	8.5	8.7	10.7	9.3
Total Hydrocarbons (ppm) ^c	< 0.1	2.5	< 0.1	< 0.9
Emission Rate ^b				
Carbon Monoxide (lbs/hr)	1.39	1.27	1.58	1.41
Total Hydrocarbons (lbs/hr)	<0.03	0.64	<0.02	<0.23

a) volume/volume

b) lbs/hr = ppm x DSCFM x molecular weight x (15.58 x 10⁻⁸)

c) ppm as propane

TABLE 2-2

SUMMARY OF MEASURED AIR POLLUTANTS
TURBINE NO. 2
ALGONQUIN GAS TRANSMISSION COMPANY
HANOVER, NEW JERSEY

Test Date Time	T-1 11/13/90 0720-0830	T-2 11/13/90 0955-1121	T-3 11/13/90 1222-1350	Average
<u>Stack Conditions</u>				
Flowrate (DSCFM)	37500	36500	36300	35400
Temperature (°F)	785	784	802	790
Moisture (%)	4.4	3.1	3.6	3.7
Oxygen (%)	17.6	17.1	17.1	17.3
<u>Pollutant Emissions</u>				
Concentration ^a				
Carbon Monoxide (ppm)	8.2	9.7	9.2	9.0
Total Hydrocarbons (ppm) ^c	< 0.1	< 0.1	< 0.1	< 0.1
Emission Rate ^b				
Carbon Monoxide (lbs/hr)	1.44	1.70	1.61	1.58
Total hydrocarbons (lbs/hr)	<0.023	0.025	<0.025	<0.025

a) volume/volume

b) lbs/hr = ppm x DSCFM x molecular weight x (15.58 x 10⁻⁸)

c) ppm as propane

TABLE 2-3

SUMMARY OF MEASURED NITROGEN OXIDE EMISSIONS
TURBINE NO. 1
ALGONQUIN GAS TRANSMISSION COMPANY
HANOVER, NEW JERSEY

Test	T-1	T-2	T-3	
Date	11/13/90	11/13/90	11/13/90	
Time	1130-1246	1400-1528	1540-1658	Average
<u>Ambient Conditions</u>				
Barometric Pressure (in Hg)	30.05	30.07	30.20	30.11
Temperature (°F)	38	42	47	42
Relative Humidity (%)	40	40	45	42
Saturation Vapor Pressure (in Hg) ^a	0.247	0.268	0.323	0.279
<u>Stack Conditions</u>				
Flowrate (DSCFM)	37500	33600	33900	34800
Temperature (°F)	778	712	785	759
Oxygen (%)	17.0	18.1	17.2	17.4
<u>Process Conditions</u>				
Fuel Flow (MMBTU/hr)	40	32	41	38
Combustor Inlet Pressure (PSIG)	122	93	122	112
Operating Load (HP)	3980	2522	3873	3458
<u>Nitrogen Oxide Emissions</u>				
<u>Concentration</u>				
Uncorrected (ppm) ^b	78.9	55.1	85.6	73.2
@15% Oxygen	125.8	116.1	136.5	126.1
@15% Oxygen & ISO Conditions	119.0	114.9	126.9	120.3
<u>Emission Rate</u>				
lbs/hr ^c	13.8	8.64	13.6	12.0

a) from table of vapor pressure in Appendix E, Chemical Engineers Handbook

b) volume/volume (dry)

c) $\text{lbs/hr} = \text{ppm} \times \text{DSCFM} \times \text{molecular weight} \times (15.58 \times 10^{-8})$

TABLE 2-4

SUMMARY OF MEASURED NITROGEN OXIDE EMISSIONS
TURBINE NO. 2
ALGONQUIN GAS TRANSMISSION COMPANY
HANOVER, NEW JERSEY

Test Date Time	T-1 11/13/90 1130-1246	T-2 11/13/90 1400-1528	T-3 11/13/90 1540-1658	Average
<u>Ambient Conditions</u>				
Barometric Pressure (in Hg)	30.14	30.14	30.14	30.14
Temperature (°F)	35	40	48	41
Relative Humidity (%)	45	45	45	45
Saturation Vapor Pressure (in Hg) ^a	0.204	0.247	0.337	0.263
<u>Stack Conditions</u>				
Flowrate (DSCFM)	33500	36500	36300	35400
Temperature (°F)	785	784	802	790
Oxygen (%)	17.6	17.1	17.1	17.3
<u>Process Conditions^d</u>				
Fuel Flow (MMBTU/hr)	41	41	41	41
Combustor Inlet Pressure (PSIG)	124	123	122	123
Operating Load (HP)	4011	3940	3918	3956
<u>Nitrogen Oxide Emissions</u>				
<u>Concentration</u>				
Uncorrected (ppm) ^b	67.3	76.8	76.3	73.5
@15% Oxygen	120.3	119.2	118.5	119.3
@15% Oxygen & ISO Conditions	115.7	112.9	109.9	112.5
<u>Emission Rate</u>				
lbs/hr ^c	10.5	13.1	13.0	12.2

a) from table of vapor pressure in Appendix E, Chemical Engineers Handbook

b) volume/volume (dry)

c) $\text{lbs/hr} = \text{ppm} \times \text{DSCFM} \times \text{molecular weight} \times (15.58 \times 10^{-8})$

d) As provided by Algonquin

3.0 PROCESS DESCRIPTION

Algonquin Gas Transmission Company operates two 3830 hp Solar Centaur Model No. CD1-CB-C307 gas turbines at their compressor station in Hanover, New Jersey. These units provide auxiliary transfer capacity to Algonquin's gas transmission network. These units have no emission control devices installed on their exhaust systems.

During each one-hour test period, each unit was operated at or near 100% capacity. The following parameters were recorded by Algonquin personnel during each test period to document each turbine's operation:

*	Operating Load	(hp)
*	Fuel Flow Rate	(ft ³ /HR)
*	Compressor Discharge Pressure	(PSIG)
*	Combustion Inlet Pressure	(PSIG)

Copies of this recorded data are included in Appendix D.

4.0 SAMPLING AND ANALYTICAL METHODS

Air pollution emission measurements were performed to determine NO_x , CO, and total hydrocarbons (THC) emission concentrations from the solar turbine exhaust. In addition, exhaust gas flowrates, moisture content, and the percent of CO_2 and O_2 in the exhaust gas were determined. Copies of data sheets used during the field effort are presented in Appendix A.

4.1 Continuous Emission Monitoring of CO, CO_2 , and O_2

Continuous emission monitoring (CEM) was performed at each exhaust duct to determine concentrations and emission rates of CO_2 , CO, and THC. A schematic of the CEM system is presented in Figure 4-1. Measurements were performed continuously for a minimum of three hours of operation on each unit.

All CEM data was recorded by a Kaye Digistrip III automatic digital data logger. The CEM system was housed in the TRC Mobile Environmental Laboratory.

Sample Conditioning System

A heated external Alundum thimble filter with a stainless steel nozzle facing away from the stack gas flow served to remove large particulate matter from the sample gas stream. The thimble filter was mounted on the end of stainless steel sampling probe. The sampling stream was drawn through one hundred (100) feet of heated ($250^\circ\text{F} \pm 25^\circ\text{F}$) Teflon sample line and through a sample conditioner to remove the moisture from the gas stream. The sample was then drawn through Teflon tubing by a leak-free Teflon double diaphragm pump to a stainless steel sample manifold with an atmospheric by-pass rotameter. The CO and CO_2 analyzers drew samples from this manifold. The total hydrocarbon analyzer drew unconditioned sample through a heated (250°F) Teflon sample line connected prior to the conditioner.

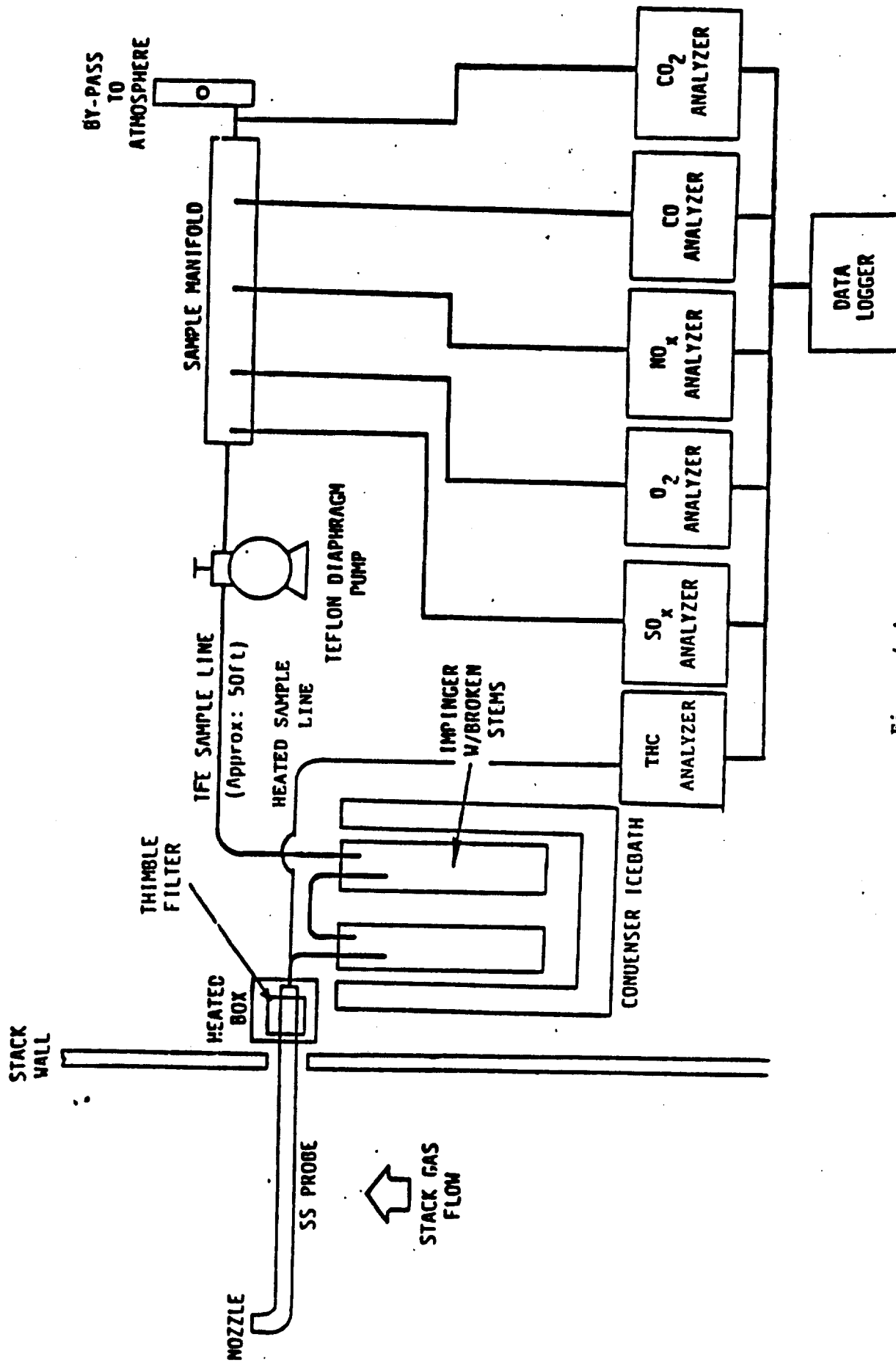


Figure 4-1
Continuous Emission Monitoring System Schematic

Continuous Monitors

Emission parameters which were monitored continuously at maximum load will be CO, CO₂, and THC. Carbon monoxide concentrations were monitored in accordance with EPA Method 10. CO₂ concentrations were measured in accordance with EPA Method 3A. THC concentrations were measured in accordance with NJ Method 3 guidelines.

A Westinghouse Model UNOR 6N non-dispersive infrared gas analyzer was used to measure CO concentrations. This analyzer operates on the measurement principle based on CO having a known characteristic absorption spectrum in the infrared range. It contains an infrared detector that uses the single non-dispersive beam technique with alternate modulations of the sample and reference cells. Radiation absorbed by CO in the sample cell produce a capacitance change in the detector which is proportional to the CO concentration.

An Infra-Red Industries, Inc. infrared CO₂ analyzer was used to monitor CO₂ emissions. This instrument operates on the principle of CO₂ having a known characteristic absorption spectra in the infrared range. Radiation absorbed by CO₂ in the sample cell produces a capacitance change in the detector which is proportional to the CO₂ concentration.

A Ratfisch Model RS55 Total Hydrocarbon Analyzer, which utilizes a flame ionization process was used to determine THC concentrations in accordance with NJ Method 3. A small amount of sample containing hydrocarbons is introduced to the system through a heated filter, sample line, and pump. The sample gas enters the heated detector bench, which contains the flame ionization detector

(FID). The resulting current is detected and amplified, and the output of the amplifier provides a signal for direct readout on a meter or for output to a recorder or computer.

Data Acquisition and Handling

All CEM data was monitored by a Kaye Instruments Digistrip III automatic data logger which recorded data on it's integral printer. Emission data will be "viewed" by the data logger every six seconds and averaged at 1- to 2-minute intervals. This enabled real-time emission data to be available on site.

CEM System Calibration

Calibrations of the CEM system were performed at the beginning and end of each test period. Calibration gases (Protocol I or NBS traceable) were introduced to the system through a 3-way valve at the back of the sample probe. Span gases for O₂, CO, NO_x, CO₂, and propane were used. Each analyzer was multi-point calibrated prior to the test program to document each instruments linearity.

4.2 Nitrogen Oxides

Triplicate measurements of NO_x and O₂, were performed on the Solar turbines during one-hour tests according to EPA Method 20. TRC used a Thermo-Electron Model 10A chemiluminescent NO/NO_x analyzer and Horiba Model PMA-200 paramagnetic oxygen analyzer to perform the measurements. The measurement system used is that described in Section 4.1. Prior to each day's sampling, TRC conducted the following measurement system performance tests or equivalent as outlined in EPA Method 20.

- * NO_x and O₂ Calibration Gas Check
- * Calibration Check^a
- * Interference Response Check
- * Residence and Response Time Check
- * NO₂ to NO Conversion Efficiency Check

This data is presented in Appendix C

A Horiba Model PMA-200 oxygen analyzer was used to determine concentrations of O₂ in the stack gas. This instrument utilizes the magnetic dumbbell sphere (paramagnetic) principle, which comparatively measures the magnetic susceptibility of a gas volume by the force acting upon a non-magnetic test body suspended in a disproportionate magnetic field. Output current is proportional to the oxygen concentration.

The Thermo-Electron NO/NO_x gas analyzer utilizes the chemiluminescent reaction of NO and O₃ (ozone) as provided by the analytical method (NO + O₃ → NO₂ + O₂).

- a. According to EPA Method 20, the following span gas calibration ranges needed to be used to calibrate the NO_x instrument; 100%-80%, 45-55%, 20%-30%. TRC's 100%-80% of span calibration gas did not yield an acceptable value. Since the increased NO_x values never exceeded the mid-level calibration gas value, Michael Papp from NJDEP approved the elimination of the high level calibration gas.

Before initiating the NO_x measurements, EPA Method 20 states that a preliminary oxygen measurement profile should be conducted with the gas turbine operated at maximum load, using 16 traverse points. The minimum sampling time at each point should be one minute plus the average system response time as outlined by EPA Method 20. The emission test consisted, however, of a 16 point traverse along the duct cross-section. Throughout the duct the oxygen concentration remained stable. Immediately following each test run, the instrument zero and calibration drift was determined using zero and mid-level calibration gases. All NO_x emissions were corrected to 15% O₂ and ISO standard conditions using the following formulae.

$$1. \quad \text{NO}_{x15\text{O}_2} = \left[\text{NO}_{x\text{meas (dry)}} \right] \left[\frac{(20.9 - 15)}{(20.9 - \text{CO}_2)} \right]$$

where:

$\text{NO}_{x\text{meas}}$ = NO_x concentration measured ppm (dry)

CO_2 = CO_2 measured (dry)

$$2. \quad \text{NO}_{x15\text{O}_2} = \left[\text{NO}_{x15\text{O}_2} \right] \left[\text{ISO E Factor} \right]$$

where:

$$\text{ISO E Factor} = \left(\frac{P_{\text{ref}}}{P_{\text{obs}}} \right)^{0.5} \left(e^{19(H_{\text{amb}} - 0.00633)} \right) \left(\frac{288^\circ\text{K}}{T_{\text{amb}}} \right)^{1.53}$$

$\text{NO}_{x15\text{O}_2}$ = ppm NO_x at 15% O_2 and ISO std. cond.

$\text{NO}_{x15\text{O}_2}$ = ppm NO_x at 15% O_2

P_{ref} = reference combustor inlet absolute pressure at 29.92 in. Hg ambient pressure, in. Hg

P_{obs} = measured combustor inlet absolute pressure at test ambient pressure, in. Hg

e = transcendental constant (2.718)

H_{amb} = ambient specific humidity

T_{amb} = ambient temperature, $^\circ\text{K}$

$$H_{\text{amb}} = \frac{1}{100} \left[\frac{P_v}{1.61 (P_{\text{obs}} - P_v)} \right]$$

P_v = saturation vapor pressure at T_{amb} , in. Hg

The calibration span value was 250 ppm for these tests. Examples of these calculations are presented in Appendix E.

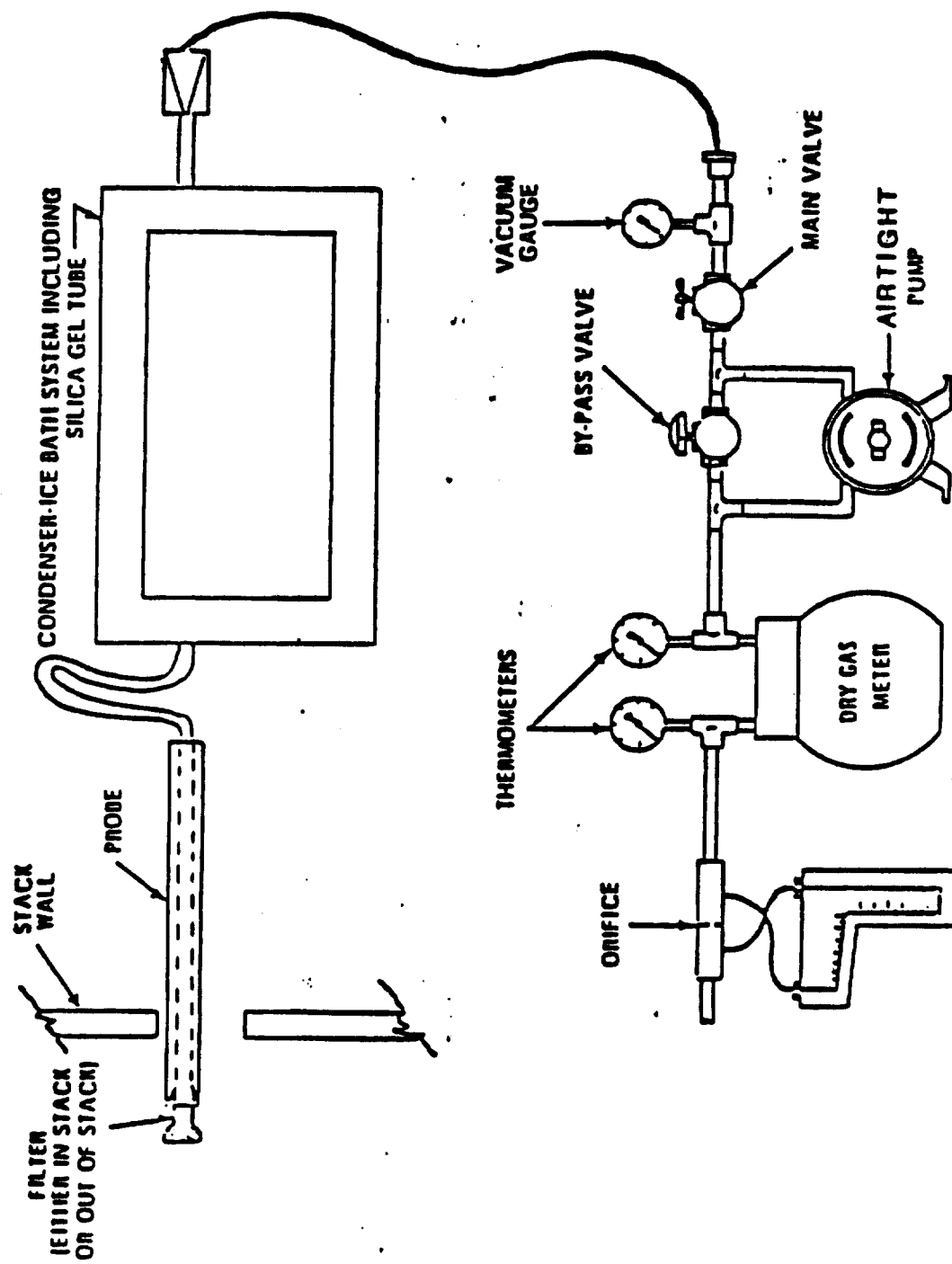


Figure 4-2 Moisture sampling train

4.3 EPA Method 4

Sample Collection

Moisture sampling was performed at each outlet using a modified EPA collection train, Method 4, similar to that described in the July 1, 1987, edition of the Federal Register. It is shown schematically in Figure 402 and consists of a heated probe, filter, a flexible Teflon umbilical line, four impingers, vacuum pump, dry gas meter, and an orifice flow meter.

The TRC modification of the standard EPA Method 4 train consisted of placing the flexible Teflon tubing between the probe and the impinger. This modification makes the sampling equipment much less awkward to handle and allows vertical orientation of the sampling probe without risk of impinger damage or loss of impinger solutions. Complete sampling train calibrations were performed before and after the compliance test program and are contained in Appendix B.

An ice bath containing four impingers was attached to the back end of the probe via a flexible Teflon umbilical tube. The first two impingers contained water, the third was dry, and the fourth contains silica gel to remove any remaining moisture. Flexible tubing, a vacuum gauge, needle valve, leak-less vacuum pump, bypass valve, dry gas meter, calibrated orifice, and a dual range inclined manometer completed the sampling train.

Sampling flow valve was adjusted with the bypass valve to maintain 0.75 cfm. Before and after each test run the sampling train was leak checked (accepted at less than 0.02 cfm). Four ports were traversed at four points during each 64-minute test period.

Sample Analysis

After the sample was collected, the sample train was leak-checked as described in EPA Method 4. The volume of moisture condensed in the first three impingers was measured to the nearest milliliter. The silica gel weight increase of the fourth impinger was also be determined to the nearest 0.5 milligram. This information along with the total volume of gas samples was used to calculated the moisture content of the exhaust gas.

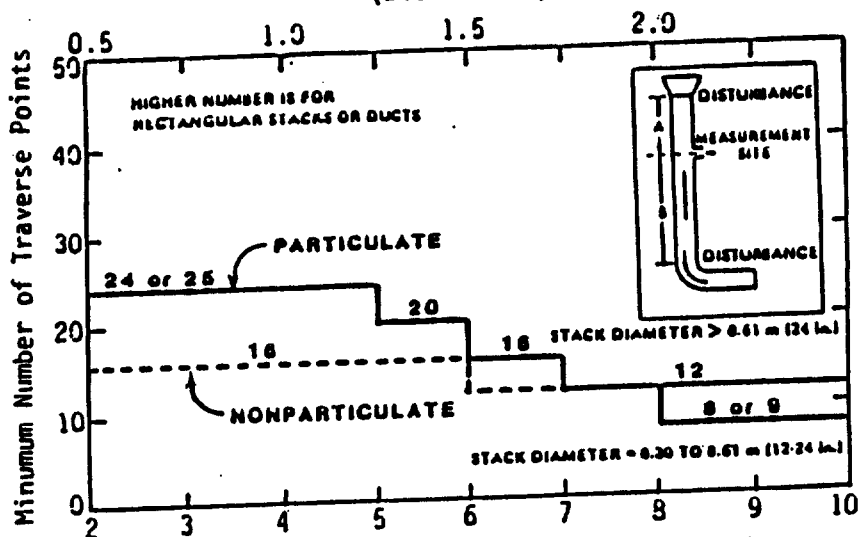
4.4 Flowrate Measurements

A velocity traverse was performed at the turbine exhaust location in accordance with EPA Methods 1 and 2. The gas velocity was measured using an S-type pitot tube and inclined water manometer. The flue gas temperature was monitored by a thermocouple attached to the pitot and connected to a potentiometer. Measurements were performed before, during, and after each test. Traverse point locations are presented in Figure 4-3.

Firm Algonquin Total Traverse Points Required 16
 Location Turbines 1 and 2 Number of Ports 4
 Diameters Upstream 0.6 Points Per Port 4
 Diameters Downstream 2.4 Traverse (Horizontal or Vertical) Horizontal

MINIMUM NUMBER OF TRAVERSE POINTS FOR PARTICULATE AND NONPARTICULATE TRAVERSES

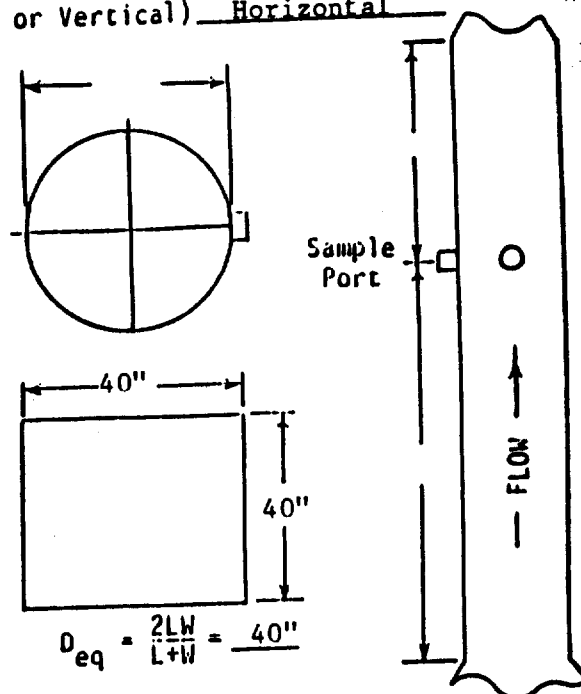
Duct Diameters Upstream from Flow Disturbance (Distance A)



Duct Diameters Downstream from Flow Disturbance (Distance B)

LOCATION OF TRAVERSE POINTS IN CIRCULAR STACKS

Point Number On A Diameter	(Percent of stack diameter from inside wall to traverse point)				
	Number Of Traverse Points On A Diameter				
	4	6	8	10	12
1	6.7	4.4	3.2	2.6	2.1
2	25.0	14.6	10.5	8.2	6.7
3	75.0	29.6	19.4	14.6	11.8
4	93.3	70.4	32.3	22.6	17.7
5		85.4	67.7	34.2	25.0
6		95.6	80.6	65.8	35.6
7			89.5	77.4	64.4
8			96.8	85.4	75.0
9				91.8	82.3
10				97.4	88.2
11					93.3
12					97.9



CROSS-SECTIONAL LAYOUT FOR RECTANGULAR STACKS

Total Traverse Points	Matrix
9	3x3
12	4x3
16	4x4
20	5x4
25	5x5

TRAVERSE POINT LOCATIONS

No.	Distance From Wall	Nipple Size	Total Distance
1	5"		
2	15"		
3	25"		
4	35"		
5			
6			
7			
8			
9			
10			
11			
12			

5.0 QUALITY ASSURANCE

TRC's quality assurance program is designed to ensure that emission measurement work is performed by qualified people using proper equipment following written procedures in order to provide accurate, defensible data. This program is based upon the EPA Quality Assurance Handbook for Air Pollution Measurement Systems, Volume II I(EPA-600/4-7-027 1b).

5.1 Methods 1, 2, and 4

TRC's measurement devices, including pitot tubes, dry gas meters, thermocouples, probes, and nozzles are uniquely identified and calibrated with documented procedures and acceptance criteria before and after each field effort. Records of all calibration data are maintained in TRC files.

Probe and sample line temperatures were maintained within 25°F of the temperatures specified. All glassware is cleaned by the following procedures prior to use for sampling when condensables are collected.

1. Acetone Rinse
2. Hot Detergent
3. Hot Water Rinse
4. Chromic Acid Soak
5. Hot Water Rinse
6. Distilled Deionized Water Rinse

5.2 CEM System

The CEM System was calibrated and leak-checked at the beginning and end of each test day. All calibration gases were NBS certified or equivalent and representative of stack gas concentration. Multipoint calibrations were performed on the analyzers prior to the field program to establish linearity.

5.3 EPA Method 20 Performance Checks

Before each test day, the following performance checks were performed:

- Calibration Gas Check

Certification sheets for this check can be found in Appendix C.

- Calibration Check

Instrument calibration checks are found in Appendix C

- Interference Response Check

Data sheets showing no interference gas response can be found in Appendix C.

- Residence and Response Time

The data sheet showing the response time is found in Appendix C

- NO₂ to NO Conversion Efficiency

A conversion efficiency test was performed in the laboratory prior to the field effort. The conversion efficiency was found to be 100%.

APPENDIX A

Field Data

METHOD 20
FIELD DATA SHEET

Firm Algonquin P_{obs} _____ in. Hg
Location HANOVER NJ T_{AMB} 40 °F
Tester JOJO SBN BTB T_{AMB} 4.4 °C
Unit #1 SN CC84068 Wet Bulb _____ °F
Date 11/13/90 Relative Humidity 40 %
Time 1130-1240 P_v 6.274 mm Hg = 159.26 in. Hg

Turbine Load MW/e	NO _x (dry) PPM	O ₂ (dry) %	CO ₂	NO _x (15%) PPM	NO _x (ISO) PPM	ISO K Factor
1130	76.0	17.0	2.5			
1140	78.0	17.0	2.5			
1156	77.7	17.0	2.5			
1200	80.2	17.0	2.5			
12142	74.0	17.3	2.3			
1220	72.5	17.3	2.4			
1230						
AVERAGE	78.9	17.0		125.8	119.0	0.946

$$1. \quad \text{NO}_{x15\% \text{ O}_2} = \left[\text{NO}_{x \text{ meas (dry)}} \right] \left[\frac{(20.9 - 15)}{(20.9 - \% \text{O}_2)} \right]$$

Where:

NO_{x meas} = NO_x concentration measured ppm (dry)

%O₂ = %O₂ measured (dry)

$$2. \quad \text{NO}_{x \text{ ISO}} = \left[\text{NO}_{x15\% \text{ O}_2} \right] \left[\text{ISO K Factor} \right]$$

Where:

$$\text{ISO K Factor} = \left(\frac{P_{\text{ref}}}{P_{\text{obs}}} \right)^{0.5} \left(\frac{19(H_{\text{amb}} - 0.00633)}{T_{\text{amb}}} \right) \left(\frac{298^\circ \text{K}}{T_{\text{amb}}} \right)^{1.53}$$

NO_{x ISO} = ppm NO_x at 15% O₂ and ISO std. cond.

NO_{x15% O₂} = ppm NO_x at 15% O₂

P_{ref} = reference combustor inlet absolute pressure at 29.92 in. Hg ambient pressure, in. Hg

P_{obs} = measured combustor inlet absolute pressure at test ambient pressure, in. Hg

e = transcendental constant (2.718)

H_{amb} = ambient specific humidity

T_{amb} = ambient temperature, °K

$$H_{\text{amb}} = \frac{\% \text{ RH}}{100} \left[\frac{P_v}{1.61 (P_{\text{obs}} - P_v)} \right]$$

P_v = saturation vapor pressure at T_{AMB}, in. Hg

TR0 - VINL STAFF ISUL² S, 1
CONTINUOUS EMISSION MONITORING
FIELD DATA SHEET

Firm Algonquin
Location Harvey, IL
Tester 80050AB

Test Number	T-1-1
Sample Loc.	Unit #1
Date	11/12/90
Time	1130 1240

Ambient Temp.	38
HEL Temp.	80
Bar. Pressure	30.05
Vacuum Gauge	11 in Hg
Pressure Gauge	~750

		INITIAL VALUES				FINAL VALUES				range & units	avg. gas (%) conc.	effluent gas (%) conc.
Analyzer	(Rack) analyzer cal.	system cal. response	system cal. bias (% of span)	system cal. bias (% of span)	system cal. response	system cal. bias (% of span)	drift (% of span)					
CO	zero	0.2	-0.4	1.1	-1.2	1.4	0.3	100%				
	upscale	41.5	36.9	4.6	36.9	4.6	0.0					
O2	zero	0.0	0.0	0.0	0.1	0.4	0.4	25%				
	upscale	22.4	22.1		22.1	1.2	1.2					
CO2	zero	0.1	0.1	0.0	0.1	0.0	0.0	20%				
	upscale	12.1	12.6	0.5	12.6	0.5	0.0					
NOx	zero	0.2	0.5	0.0	-0.2	0.2	0.1	250 PPM				
	upscale	146.0	137.2	8.8	137.0	8.9	1.7					
SO2	zero											
	upscale											
THC	zero	0.1	-0.2	0.3	-0.3	0.4	0.1	0-100 PPM				
	upscale	9.6			8.0	1.6	1.0					
				+5%		+5%	+3%					

LEAK CHECK			
Analyzer	response	cal. back cal. upstream of analyzer	bias check (% of span)
CO zero	0.2		
upscale			
NO _x zero	0.0	0.2	
upscale	142.5	146.0	+ 5 %

Calibration Gases

	Low Cal	Mid Cal	High Cal	Mid	High	Tank ID#
N ₂	71.2	14.3	223.1	ALM008207/ALC5019/112066		0820
O ₂	—	11.0	22.06	AAL 20877/ALM5152		
CO ₂	—	5.0	12.0	ALM009709/ALC3934		
CO _{NOx}	—	10.1	41.6	24116 / 2L1125		
SO ₂	—	—	—	—		
TBC ₂₅	—	9.67	104	361716/ALC8734		361274

$$\begin{aligned} \text{system cal.} &= \frac{\text{cal resp.}}{\text{span (range)}} \times 100 \\ \text{drift} &= \frac{\text{final system} - \text{initial system}}{\text{span (range)}} \times 100 \\ \text{C} &= \text{average gas conc.} \\ Q_{\text{ps}} &= \text{actual cal gas upscale} \\ C_0 &= \text{avg. of zero gas for bias system cal} \\ C_m &= \text{avg. of upscale for bias system cal} \\ C_g &= \text{effluent gas} \end{aligned}$$

METHOD 20
FIELD DATA SHEET

Firm Algonquin P_{obs} _____ in. Hg
Location Haver NJ T_{amb} 42 °F
Tester T-1-2 T_{amb} _____ °K
Unit #1 Wet Bulb 50 °F
Date 11/13/90 Relative Humidity 40 %
Time 1400-1528 P_v 6.822 mm Hg

Turbine Load MW/s	NO _x (dry) PPM	O ₂ (dry) %	NO _x (15%) PPM	NO _x (ISO) PPM	ISO K Factor
1400	74.0	17.5	2.2		
1410					
AVERAGE	55.1	18.1	116.1	114.9	0.990

$$1. \quad NO_{x_{15\% O_2}} = \left[NO_{x_{meas}} (dry) \right] \left[\frac{(20.9 - 15)}{(20.9 - \%O_2)} \right]$$

Where:

NO_{x_{meas}} = NO_x concentration measured ppm (dry)

%O₂ = %O₂ measured (dry)

$$2. \quad NO_{x_{ISO}} = \left[NO_{x_{15\% O_2}} \right] \left[ISO \text{ K Factor} \right]$$

Where:

$$ISO \text{ K Factor} = \left(\frac{P_{ref}}{P_{obs}} \right)^{0.5} \left(\frac{19(H_{amb} - 0.00633)}{e} \right) \left(\frac{288^\circ K}{T_{amb}} \right)^{1.53}$$

NO_{x_{ISO}} = ppm NO_x at 15% O₂ and ISO std. cond.

NO_{x_{15% O₂}} = ppm NO_x at 15% O₂

P_{ref} = reference combustor inlet absolute pressure at 29.92 in. Hg ambient pressure, in. Hg

P_{obs} = measured combustor inlet absolute pressure at test ambient pressure, in. Hg

e = transcendental constant (2.718)

H_{amb} = ambient specific humidity

T_{amb} = ambient temperature, °K

$$H_{amb} = \frac{\% RH}{100} \left[\frac{P_v}{1.61 (P_{obs} - P_v)} \right]$$

P_v = saturation vapor pressure at T_{amb}, in. Hg

TRC IRON AL ULTI IN
CONTINUOUS EMISSION MONITORING
FIELD DATA SHEET

Firm Algonquin
Location Haverhill NJ
Tester JOE SAN ANS

Test Number T-1-2
Sample Loc. Unit #1
Date 11/13/50
Time 1400-1525

Ambient Temp. 42
REL Temp. 86
Bar. Pressure 30.07
Vacuum Gauge 11
Pressure Gauge 706

INITIAL VALUES				FINAL VALUES			
(Rack)	analyzer cal.	system cal. response (% of span)	system cal. bias (% of span)	system cal. response (% of span)	system cal. bias (% of span)	drift (% of span)	range & avg. effluent gas (C) conc.
CO zero	-1.8	-1.2	0.0	-1.3	0.1	0.1	100 ppm
CO upscale	41.3	36.9	4.4	36.3	5.0	0.6	
O ₂ zero	0.0	0.1	0.1	0.0	0.0	0.4	25%
O ₂ upscale	23.5	22.1	1.4	22.0	2.0	0.4	
CO ₂ zero	0.1	0.1	0.0	0.1	0.0	0.5	20%
CO ₂ upscale	12.5	12.6	0.5	12.5	0.3	0.1	250 ppm
NO _x zero	-0.7	-0.2	0.7	0.0	4.3	0.1	
NO _x upscale	115.7	133.0	5.0	135.0			
SO ₂ zero							
SO ₂ upscale							
THC zero	0.2	-0.3					
THC upscale	9.1	8.0					
			± 5%		± 5%	± 3%	

LEAK CHECK

cal. back cal. upstream
of analyzer of analyzer bias check
response response (% of span)

Analyzer	response	response	response
CO zero			
CO upscale			
NO _x zero			
NO _x upscale			± 5%

$$\text{system analyzer cal} = \frac{\text{resp. cal}}{\text{span (range)}} \times 100$$

$$\text{system cal.} = \frac{\text{resp. cal}}{\text{span (range)}} \times 100$$

$$C_g = (\bar{C} - \bar{C}_0) \frac{C_{ma}}{C_m - C_0}$$

$$C_g = \text{effluent gas}$$

$$C = \text{average gas conc.}$$

$$C_{ma} = \text{actual cal gas upscale}$$

$$C_0 = \text{avg. of zero gas for bias system cal}$$

$$C_m = \text{avg. of upscale for bias system cal}$$

$$\text{drift} = \frac{\text{final system} - \text{initial system}}{\text{cal resp. cal resp.}} \times 100$$

$$\text{drift} = \frac{\text{cal resp. cal resp.}}{\text{span (range)}} \times 100$$

Calibration Gases

Tank ID#

Mid High

Mid Cal High Cal

CO

O₂

CO₂

NO_x

SO₂

THC_{as}

Firm	Algarquin
Location	Harvey, NJ
Tester	BOSSA, B

Test Number	Sample Loc.	Date	Time
-------------	-------------	------	------

Ambient Temp.	47
HEL Temp.	80
Bar. Pressure	30.20
Vacuum Gauge	11
Pressure Gauge	290

FIELD DATA SHEET -

Analyzer	(Rack) analyzer cal.	INITIAL VALUES			FINAL VALUES			range & units	avg. gas (C) conc.	effluent gas (C) conc.
		system cal. response	system cal. bias (% of span)	system cal. bias (% of span)	system cal. response	system cal. bias (% of span)	drift (% of span)			
CO	zero	0.2	0.1	0.1	-0.3					
	upscale	8.3	7.6	0.7	7.1			1.24		
O2	zero	9.0	9.1	0.1	0.0					
	upscale	12.3	22.1	0.2	22.0			1.24		
CO2	zero	0.1	0.2	0.5	0.2			1.24		
	upscale		12.0		12.0					
NOx	zero	0.2	0.7	0.1	0.7					
	upscale	143.8	142.8	0.1	150.2		3.0	1.24		
SO2	zero									
	upscale									
THC	zero	0.0	0.4		-0.2					
	upscale	9.7	9.7		9.1			1.24		
				+ 5.0		+ 5.0	+ 3.0			

LEAK CHECK

Analyzer	cal. back of analyzer response	cal. upstream of analyzer response	bias check (% of span)
CO zero			
upscale			
NO _x zero			
upscale			
			+ 5 %

$$\text{system cal.} = \frac{\text{system analyzer cal.}}{\text{resp. span (range)}}$$

$$\text{drift} = \frac{\text{final system} - \text{initial system}}{\text{span (range)}} \times \text{cal resp.}$$

$$\frac{m_1 - m_2}{m_1 + m_2} = (1 - \epsilon)$$

Cg - effluent gas

C - average gas conc.

Q_{gas} = actual cal gas upscale

to - avg. of zero gas for

bias system cal

C_m - avg. of upscale for

business system cal

Calibration Cases

	<u>Mid Cal</u>	<u>High Cal</u>	<u>Tank ID#</u>
CO	_____	_____	____/____
O ₂	_____	_____	____/____
CO ₂	_____	_____	____/____
NO _x	_____	_____	____/____
SO ₂	_____	_____	____/____
TBC...	_____	_____	____/____

Firm	<u>Algonquin</u>
Location	<u>Hammer NJ</u>
Tester	<u>Bob Sen ASB</u>

Ambient Temp. 35
 MEL Temp. 80
 Bar. Pressure 30.14
 Vacuum Gauge 11
 Pressure Gauge 200.14

(Rack)	INITIAL VALUES			FINAL VALUES			effluent gas (C ₂) conc.
	analyzer response	cal. response (% of span)	system cal. bias (% of span)	analyzer response	cal. response (% of span)	system cal. bias (% of span)	
Analyzer response	100	100	100	100	100	100	avg. gas (C ₂) conc.

Analysis	Response	% of Span	Response	% of Span	Response	% of Span	Response	% of Span
CO	zero	-0.2	0.0	0.2	-0.1	0.2	0.5	
	upscale	41.5	33.5	3.0	13.2	12.0	0.8	100 mm
O ₂	zero	0.1	0.2	0.4	8.2	0.4	0.0	
	upscale	22.7	22.1	2.4	22.3	1.6	0.8	25 mm
CO ₂	zero	0.1	0.1	0.0	0.1	0.0	0.0	
	upscale	12.1	11.9	1.0	12.0	0.5	0.5	20 mm
NO _x	zero	0.0	0.2	0.1	0.0	0.0	0.1	
	upscale	142.7	134.5	3.3	134.2	3.4	0.1	25 mm
SO ₂	zero							
	upscale							
THC	zero	0.2	-0.2	0.4	0.0	0.2	0.2	
	upscale	9.7	8.9	0.8	10.3	0.6	1.4	100 mm
				± 5.0		± 5.0	± 3.0	

LEAK CHECK

Analyzer	cal. back of analyzer response	cal. upstream of analyzer response	bias check (% of span)
CO zero			
upscale			
NO _x zero			
upscale			
			+ 5 %

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$$\text{system cal.} = \frac{\text{resp. resp.}}{\text{span (range)}} \times 100$$

C - average gas conc.

Q_{gas} = actual cal gas upscale

C_0 = avg. of zero gas for
bias system cal

C_m = avg. of upscale for
bias system cal

Calibration Gases

	<u>Mid Cal</u>	<u>High Cal</u>	<u>Tank ID#</u>
	<u>Mid</u>	<u>High</u>	
CO	_____	_____	____/____
O ₂	_____	_____	____/____
CO ₂	_____	_____	____/____
NO _x	_____	_____	____/____
SO ₂	_____	_____	____/____
THC _{as}	_____	_____	____/____

TRC IRO CAL IULT
CONTINUOUS EMISSION MONITORING
FIELD DATA SHEET

Firm Algonquin
Location Algonquin
Tester Bob San AIB

Test Number T-2-2
Sample Loc. Unit 2
Date 11/14/90
Time 0955-1031

Ambient Temp. 40
REL Temp. 82
Bar. Pressure 30.11
Vacuum Gauge 11
Pressure Gauge 200

INITIAL VALUES				FINAL VALUES			
(Rack)							
Analyzer	analyzer cal.	system response (% of span)	system cal. bias (% of span)	system cal. response (% of span)	system cal. bias (% of span)	drift (% of span)	range & units
CO zero	-0.2	-0.7	0.3	-0.7	0.3	0.2	
CO upscale	41.5 / 9.2	11.2	0.0	11.2	0.0	0.0	100 ppm
O2 zero	0.1	0.2	0.4	0.2	0.4	0.8	
O2 upscale	22.7	22.3	1.6	22.1	2.4	0.8	25%
CO2 zero	0.1	0.1	0.0	0.1	0.0	0.0	
CO2 upscale	12.1	12.0	0.4	12.0	0.4	0.0	20%
NOx zero	0.0	0.0	0.0	0.2	0.1	0.1	
NOx upscale	142.7	134.2	3.4	134.7	3.2	0.2	250 ppm
SO2 zero							
SO2 upscale							
THC zero	0.7	0.0	0.2	0.5	0.3	0.5	
THC upscale	9.7	9.3	0.4	11.7	2.0	0.2	100 ppm

LEAK CHECK			Calibration Gases			Tank ID#		
Analyzer	cal. back of analyzer response	cal. upstream of analyzer response	Mid Cal	High Cal	Mid	High	Mid	High
CO zero								
CO upscale								
NOx zero								
NOx upscale								
system analyzer cal								
system cal. = $\frac{\text{final system} - \text{initial system}}{\text{cal resp.} - \text{cal resp.}} \times 100$								
drift = $\frac{\text{final system} - \text{initial system}}{\text{cal resp.} - \text{cal resp.}} \times 100$								

C = average gas conc.
Q_{as} = actual cal gas upscale
C₀ = avg. of zero gas for bias system cal
C_m = avg. of upscale for bias system cal

$$\text{system cal.} = \frac{\text{resp.} - \text{resp.}}{\text{span (range)}} \times 100$$

$$\text{drift} = \frac{\text{final system} - \text{initial system}}{\text{cal resp.} - \text{cal resp.}} \times 100$$

TRM / INQ TALL SULT 3.1
CONTINUOUS EMISSION MONITORING
FIELD DATA SHEET

Firm Algonquin
Location Hanover NJ
Tester SSN AB

Test Number T-2-3
Sample Loc. UNIT #2
Date 11/14/90
Time 1222-1350

Ambient Temp. 48
REL Temp. 80
Bar. Pressure 30.14
Vacuum Gauge 11
Pressure Gauge 200

INITIAL VALUES				FINAL VALUES			
Analyzer	(back) analyzer cal.	system cal. response (% of span)	system cal. bias (% of span)	system cal. response (% of span)	system cal. bias (% of span)	drift (% of span)	range & units
CO zero	-0.2	-0.5	0.3	-0.3	2.2	0.7	1.0 ppm
CO upscale	91.5	7.2	2.0	7.3	0.1	0.1	15%
O2 zero	0.1	0.0	0.1	0.0	1.8	0.1	20%
O2 upscale	22.7	22.1	7.4	22.0	0.0	0.0	20%
CO2 zero	0.1	0.1	0.0	0.1	1.0	0.3	20%
CO2 upscale	12.1	12.0	0.3	11.9	0.3	0.2	20%
NOx zero	0.0	0.2	0.1	0.7	3.9	0.7	20%
NOx upscale	142.7	134.7	3.2	133.0	0.6	0.3	100 ppm
SO2 zero	0.2	0.5	0.3	0.8	3.5	1.5	
SO2 upscale	9.7	11.7	2.0	13.2	+5%	+3%	

Calibration Gases

	Mid Cal	High Cal	Tank ID
CO			
O2			
CO2			
NOx			
SO2			
THC _{as}			

LEAK CHECK

Analyzer	cal. back of analyzer response	cal. upstream of analyzer response	bias check (% of span)
CO zero			
CO upscale			
NOx zero			
NOx upscale			+5%

$$\text{system analyzer cal} = \frac{\text{resp. cal}}{\text{span (range)}} \times 100$$

$$\text{system cal.} = \frac{\text{resp. cal}}{\text{span (range)}} \times 100$$

$$\text{drift} = \frac{\text{final system} - \text{initial system}}{\text{cal resp. cal resp.}} \times 100$$

C = average gas conc.
C_{as} = actual cal gas upscale
C₀ = avg. of zero gas for bias system cal
C_m = avg. of upscale for bias system cal



Environmental
Consultants, Inc.

EPA Method 13

FIELD DATA SHEET

Monograph
C Factor

Pitot Coefficient 0.84
Orifice ΔH 1.86
Test Start Time 11:30
Test Final Time 12:40
Leak Test Start 0.002 CFM
Leak Test Final 0.002 CFM

Nozzle No. & Dia. 0-8 in.
Assumed Moisture 0 %
Test Duration 6.4 min.
Traverse Point Interval 4 min.
Probe Heater Setting 350 °F
Filter Temp. Setting 0 °F
Dry Gas Meter Y 1.1

Orifice No. 0-8
Ambient Temp. 70 °F
Bar. Press. 30.05 in. Hg
Probe Ident. No. 501
Filter Ident. No. 0
Duct Area 20.20 ft²

Firm Name Allegiant
Plant Location NT
Test Number 1-1-1
Sampling Location Boiler #1
TRC Project No. 7638
Date 11-18-90
Tester AB

Port	Point	Time Min.	Velocity AP In H ₂ O	ΔH In H ₂ O	T_m In °F	T_m Out °F	P Stack in H ₂ O	T_{Stack} OF	Gas Sample Volume cu. ft.	P R O B E	Cyc. Angle	Heater Box Temp.	Temp. of Gas Leaving Condenser °F	Pump Vac. in Hg	Probe Temp. °F	O ₂ %	Orsat Flow-Rate (1pm) (SCFH)	F.O. Temp °F
1	1	0.0	190	186	41	41		762	277.5				45	3.5	258			
2	2	0.1	225	186	41	41		777	287.5				42	3.5	371			
3	3	0.5	312	186	43	42		780	285.6				41	3.5	427			
4	4	1.2	312	186	43	42		781	288.5				41	3.5	424			
5	5	1.6	261	186	44	43		781	291.8				41	3.5	363			
6	6	2.0	280	186	44	43	1.18	784	295.6				41	3.5	357			
7	7	2.4	280	186	44	43		786	298.7				41	3.5	358			
8	8	2.8	206	186	44	43		786	301.7				42	3.5	348			
9	9	3.3	280	186	44	43		788	304.6				41	3.5	347	334		
10	10	3.6	295	186	45	45		780	307.7				42	3.5	348	304		
11	11	4.0	270	186	45	44		779	310.8				42	3.5	322			
12	12	4.4	250	186	46	44		777	313.8				42	3.5	337			
13	13	4.8	250	186	46	44		768	316.9				42	3.5	240			
14	14	5.2	245	186	45	45		772	319.9				42	3.5	296			
Average			$\Sigma \Delta P$															

Orsat Bag Sample
Triplicate Analysis, %

CO ₂	O ₂	CO	H ₂

COMMENTS:

H₂O Collected 30.0 ml

SG Condition 7.0 mm

SG Weight 7.0 mm

Total Volume Collected 7.0 ml

Nozzle No. & Dia.	—	in.
Assumed Moisture	3	%
Test Duration	67	min.
Traverse Point Interval	—	min.
Probe Heater Setting	250	°F
Filter Temp. Setting	—	°F
Dry Gas Meter Y	101	

Nomograph
 C Factor _____
 Pitot Coefficient 0.84
 Orifice C_{dA} 1.80
 Test Start Time 1130
 Test Final Time 1246
 Leak Test Start 0.002 C_{dA} 15 "Hg
 Leak Test Final 0.002 C_{dA} 15 "Hg

CO ₂	O ₂	CO	N ₂

H ₂ O Collected	ml
SG Condition	
SG Weight	g
Total Volume Collected	ml

COMMENTS:

338



EPA Method 2.2

FIELD DATA SHEET

Firm Name Albuquerque
Plant Location 15
Test Number 7-2-1
Sampling Location 5.10 #1
TRC Project No. 7638
Date 11-13-90
Tester ASB

Orifice No. D8
Ambient Temp. 75 °F
Bar. Press. 30.5 "Hg
Probe Ident. No. 30
Filter Ident. No. 30
Duct Area 20" x 20" ft²

Nozzle No. & Dia. 3 in.
Assumed Moisture 60 min.
Test Duration 60 min.
Traverse Point Interval 250 °F
Probe Heater Setting 250 °F
Filter Temp. Setting 250 °F
Dry Gas Meter Y 601

Monograph C Factor 1.84
Pilot Coefficient 1.84
Orifice dh 1.84
Test Start Time 14:00
Test Final Time 15:24
Leak Test Start 12:22 CFM 15 "Hg
Leak Test Final 0.002 CFM 5 "Hg

Port	Point	Time Min.	Velocity AP in H ₂ O	ΔH in H ₂ O	T _M in °F	T _M out °F	P Stack in H ₂ O	T Stack of	Gas Sample Volume cu. ft.	P R O B E	Heater Box Temp.	Temp. of Gas Leaving Condenser °F	Pump Vac. in Hg	Probe Temp. °F	O ₂ %	Orsat Flow-rate (lpm) (SCFH)	F.O. Temp °F
4	1	10:20	186	186	46	45		788	332.71			43	3.0	265			
	2	10:23	186	186	46	45		788	336.24			42	3.0	285			
	3	10:23	186	186	46	45		788	339.30			41	3.0	290			
(147)	4	10:23	186	186	47	46		787	342.45			41	3.0	300			
(148)	1	10:31	186	186	47	46		789	345.53			41	3.0	257			
	2	10:32	186	186	47	46		762	348.89			41	3.0	285			
(149)	3	10:34	186	186	47	46		740	352.05			41	3.0	297			
(150)	4	10:35	186	186	47	46		706	355.17			41	3.0	301			
	1	10:37	186	186	47	46		662	358.30			41	3.0	258			
	2	10:38	186	186	47	46		671	361.39			41	3.0	281			
	3	10:39	186	186	47	46		638	364.51			41	3.0	287			
	4	10:40	186	186	47	46		634	367.67			41	3.0	296			
(151)	1	10:41	186	186	47	46		625	370.81			41	3.0	203			
(152)	2	10:42	186	186	47	46		622	377.23			41	3.0	259			
Average		Σ-ΔP		186													

H₂O Collected _____ ml
SG Condition _____
SG Weight _____ gm
Total Volume Collected _____ ml

Orsat Bag Sample
Triplicate Analysis.1

CO ₂	O ₂	CO	H ₂

COMMENTS:



Part 2

EPA Method 19

FIELD DATA SHEET

Firm Name Allegiance
Plant Location 25
Test Number 1-2
Sampling Location Boiler #1
TRC Project No. 7638
Date 11/14/50
Tester ATB

Orifice No. D8
Ambient Temp. 45 °F
Bar. Press. 30.05 "Hg
Probe Ident. No. 301
Filter Ident. No. —
Duct Area 20x20 ft²

Nozzle No. & Dia. — in.
Assumed Moisture 3
Test Duration 64 min.
Traverse Point Interval 4 min.
Probe Heater Setting 250 °F
Filter Temp. Setting — °F
Dry Gas Meter Y 1.01

Nomograph
C Factor —
Pitot Coefficient 0.84
Orifice ΔH_A 1.80
Test Start Time 1400
Test Final Time 1528
Leak Test Start 0.002 CPM 15 "Hg
Leak Test Final 0.002 CPM 6 "Hg

Port	Point	Time Min.	Velocity ΔP in H ₂ O	ΔH in H ₂ O	T _M in °F	T _M out °F	P _{Stack} in H ₂ O	T _{Stack} °F	Gas Sample Volume cu. ft.	P R O B E	Cyc. Angle	Heater Box Temp.	Temp. of Gas Leaving Condenser °F	Pump Vac. in Hg	Probe Temp. °F	O ₂ %	Drsat Flow-Rate (1pm) (SCFH)	F.O. Temp °F
	3	26	0.81	1.86	47	46	-0.77	620	37.740									
	4	60							38.056									
Average			$\Sigma \Delta P$	1.86	47	46	-0.77	712	47.85									277

H₂O Collected 21 ml
SG Condition Good
SG Weight 8.4 gm
Total Volume Collected 39.4 ml

Orsat Bag Sample
Triplicate Analysis, %

CO ₂	O ₂	CO	H ₂

COMMENTS: _____



Environmental
Consultants, Inc.

EPA Method 19

FIELD DATA SHEET

Monograph
C Factor _____
Pilot Coefficient 0.87
Orifice ΔH_a 1.86
Test Start Time 15:40
Test Final Time 17:05
Leak Test Start 0200 CFM 10 "Hg
Leak Test Final 0202 CFM 5 "Hg

Nozzle No. & Dia. _____ in.
Assumed Moisture _____
Test Duration 64 min.
Traverse Point Interval 4 min.
Probe Heater Setting 250 °F
Filter Temp. Setting _____ °F
Dry Gas Meter Y 1.01

Orifice No. P-8
Ambient Temp. 55 °F
Bar. Press. 30.02 "Hg
Probe Ident. No. 703
Filter Ident. No. _____
Duct Area 20x20 ft²

Firm Name Alcon
Plant Location NJ
Test Number 7-3
Sampling Location Water 1
TRC Project No. 7683
Date 11-14-70
Tester MD

Port	Point	Time Min.	Velocity ΔP in H ₂ O	ΔH in H ₂ O	T_M in °F	T_M out °F	P Stack in H ₂ O	T Stack °F	Gas Sample Volume cu. ft.	P R O B E	Cyc. Angle β	Heater Box Temp.	Temp. of Gas Leaving Condenser °F	Pump Vac. in Hg	Probe Temp. °F	O ₂ %	Orsat Flow-rate (1pm) (SCFH)	F.O. Temp °F
1	1	6:27	186	186	55	55		748	53115				44	35	346			
2	2	4:26	186	186	54	54		768	53767				44	35	342			
3	3	8:24	186	186	54	54		770	54115				44	35	342			
4	4	12:23	186	186	55	54		779	54463				48	35	342			
1	1	16:20	186	186	55	54		792	54809				47	35	342			
2	2	20:23	186	186	54	54		793	55153				49	35	342			
3	3	24:21	186	186	55	54		789	55488				50	35	342			
4	4	28:21	186	186	55	57		790	55800				50	30	342			
1	1	32:26	186	186	54	53		797	56111				48	30	342			
2	2	36:25	186	186	54	53		796	56412				49	30	342			
3	3	40:21	186	186	53	53		797	56745				49	30	342			
4	4	44:21	186	186	53	53		794	57050				49	30	342			
1	1	48:16	186	186	53	53	-14	794	57363				49	30	342			
2	2	52:17	186	186	52	53		794	57673					30	342			
Average		Σ-ΔP																

Orsat Bag Sample
Triplicate Analysis, %

CO ₂	O ₂	CO	N ₂

H₂O Collected 37 ml

SG Condition 10 ml

SG Weight 47 ml

Total Volume Collected

COMMENTS:



EPA Method 2.2

FIELD DATA SHEET

Firm Name Alcon
Plant Location KT
Test Number 7-3
Sampling Location Boiler
TRC Project No. 7638
Date 11/14/90
Tester ATB

Orifice No. D8
Ambient Temp. 55 °F
Bar. Press. 30.20 "Hg
Probe Ident. No. 302
Filter Ident. No.
Duct Area 20x20 ft²

Nozzle No. & Dia. in.
Assumed Moisture 3
Test Duration 64 min.
Traverse Point Interval 4 min.
Probe Heater Setting 250 °F
Filter Temp. Setting °F
Dry Gas Meter Y 101

Monograph
C Factor

Pitot Coefficient 0.84
Orifice ΔH 1.80
Test Start Time 1540
Test Final Time 1700
Leak Test Start 0.002 CFM
Leak Test Final 0.002 CFM

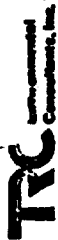
Port	Point	Time Min.	Velocity ΔP in H ₂ O	ΔH in H ₂ O	T_M in °F	T_M out °F	P Stack in H ₂ O	T Stack °F	Gas Sample Volume cu. ft.	P R O Angle	Heater Box Temp.	Temp. of Gas Leaving Condenser °F	Pump Vac. in Hg	Probe Temp. °F	O ₂ %	Orsat Flow Rate (lpm) (SCFH)	F.O. Temp °F
		3	56	110	186	52		790	979	00		50	30	34			
		4	60	100	186	52		780	583	00		51	30	34			
			67						586	16							
Average			Σ-ΔP	186	54		-140	786	52.01								

Orsat Bag Sample
Triplicate Analysis

CO ₂	O ₂	CO	H ₂

COMMENTS:

H₂O Collected ml
SG Condition
SG Weight
Total Volume Collected ml



EPA Method 3

FIELD DATA SHEET

Firm Name Akarys
Plant Location AT
Test Number T-1
Sampling Location Boiler
TSC Project No. 7633
Date 11-14-90
Tester ASD

Orifice No. D-8
Ambient Temp. 36 °F
Bar. Press. 30.14 "Hg
Probe Ident. No. 302
Filter Ident. No. —
Duct Area 20.870 ft²

Nozzle No. & Dia. — in.
Assumed Moisture 3
Test Duration 64 min.
Traverse Point Interval 4 min.
Probe Heater Setting 750 °F
Filter Temp. Setting — °F
Dry Gas Meter Y 1.01

Monograph C Factor —
Pitot Coefficient .84
Orifice M_A 1.86
Test Start Time 730
Test Final Time 857
Leak Test Start 0.008 CRM 15 "Hg
Leak Test Final 0.007 CRM 6 "Hg

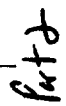
Port	Point	Time Min.	Velocity AP in H ₂ O	ΔH in H ₂ O	T _M in °F	T _M out °F	P Stack in H ₂ O	T Stack °F	Gas Sample Volume cu. ft.	P R O B E	Cyc. Angle	Heater Box Temp.	Temp. of Gas Leaving Condenser °F	Pump Vac. in Hg	Probe Temp. °F	O ₂ %	Orsat Flow-rate (1pm) (SCFH)	F.O. Temp °F
1	1	00245	186	37	37	-1.9	780	35413					35	4.5	247			
2	2	40250	186	37	37		780	38760					37	4.5	246			
3	3	80240	186	39	37		781	39063					41	4.5	73			
4	4	120240	186	39	38		783	39445					40	4.5	77			
1	1	160230	186	39	38		786	39673					40	4.5	86			
2	2	200230	186	39	38	-1.70	786	40000					41	4.5	270			
3	3	240240	186	40	38		786	40290					43	4.5	361			
4	4	280200	186	40	38		785	40596					43	4.5	348			
1	1	320240	186	39	38		786	40903					41	4.5	234			
2	2	360245	186	40	38	-1.20	785	41215					42	4.5	286			
3	3	400230	186	40	34		786	41523					43		296			
4	4	440210	186	41	39		788	41826					44	4.5	344			
1	1	480205	186	40	39		787	42128					40	4.5	340			
2	2	520170	186	40	39		788	42437					43	4.5	340			
Average		Σ-ΔP																

Orsat Bag Sample Triplicate Analysis, 1

CO ₂	O ₂	CO	N ₂

H₂O Collected 65.45 mlSG Condition 7.8 mmSG Weight 52.8 mlTotal Volume Collected 52.8 ml

COMMENTS:



FIELD DATA SHEET

Orifice No. D8
Ambient Temp. 36 °F
Bar. Press. 30.14 "Hg
Probe Ident. No. 302
Filter Ident. No. —
Duct Area 20220 ft²

Nomograph C Factor	Pitot Coefficient	Orifice ΔH	Test Start Time	Test Final Time	Leak Test Start	Leak Test Final
	0.84	1.80	730	857	900.8	0002
					15	6
					CPM	CPM

[illegible]

49.45

H ₂ O Collected	ml
SG Condition	_____
SG Weight	_____
Total Volume Collected	ml

**Orsat Bag Sample
Triplicate Analysis.1**

CO_2	O_2	O_3	N_2

COMMENTS:



TRC
TESTING & RESEARCH
CONSULTANTS, INC.

EPA Method 2.2

FIELD DATA SHEET

Nomograph
C Factor _____
Pitot Coefficient 1.81
Orifice dh_o 1.86
Test Start Time 9:55
Test Final Time 11:21
Leak Test Start 11:22 dh_o 5 dh_o
Leak Test Final 11:22 dh_o 5 dh_o

Nozzle No. & Dia. _____ in.
Assumed Moisture 3
Test Duration 64 min.
Traverse Point Interval 4 min.
Probe Heater Setting 250 $^{\circ}F$
Filter Temp. Setting _____ $^{\circ}F$
Dry Gas Meter Y 101

Firm Name Albuquerque
Plant Location AS
Test Number T-2
Sampling Location Boiler 2
TRC Project No. 7638
Date 11-14-92
Tester MS

Port	Point	Time Min.	Velocity ΔP in H ₂ O	dh in H ₂ O	T_M in $^{\circ}F$	T_M out $^{\circ}F$	P_{Stack} in H ₂ O	T_{Stack} $^{\circ}F$	Gas Sample Volume cu. ft.	P R O B E	Cyc. Angle $^{\circ}$	Heater Box Temp. $^{\circ}F$	Temp. of Gas Leaving Condenser $^{\circ}F$	Pump Vac. in Hg	Probe Temp. $^{\circ}F$	O ₂ %	Orsat Flow-rate (lpm) (SCFH)
1	1	10	185	186	44	42		672	433	82			40	30	105		
2	2	11	160	186	43	41	-140	782	430	07			40	30	140		
3	3	18	220	186	43	42		788	440	16			43	30	244		
4	4	12	225	186	44	42		790	443	25			44	30	270		
1	1	16	330	186	44	42		797	446	30			43	30	210		
2	2	18	335	186	44	43		796	449	45			44	30	170		
3	3	24	220	186	45	43		797	452	56			46	30	281		
4	4	25	210	186	45	43	-150	795	455	70			46	30	270		
1	1	33	360	186	45	44		798	458	77			43	30	90		
2	2	34	350	186	45	44		797	461	84			45	30	290		
3	3	40	230	186	46	44		796	464	95			47	30	91		
4	4	41	240	186	46	45	-190	797	468	05			47	30	87		
1	1	45	180	186	46	45		786	471	28			44	30	83		
2	2	51	190	186	47	45		785	474	26				30	182		
Average		$\Sigma \Delta P$															

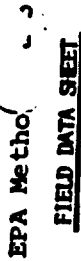
49.701

Orsat Bag Sample
Triplicate Analysis

CO ₂	O ₂	CO	N ₂

H₂O Collected 27 ml
SG Condition 9
SG Weight 36
Total Volume Collected 36 ml

COMMENTS:



Office No. 28
Ambient Temp. 45 °F
Bar. Press. 30.14 "Hg
Probe Ident. No. 382
Filter Ident. No. —
Duct Area 20 x 20 ft²

Nozzle No. & Dia. in.
Assumed Moisture 3 %
Test Duration 64 min.
Traverse Point Interval 4 min.
Probe Heater Setting 250 °F
Filter Temp. Setting — °F
Dry Gas Meter Y 1.01

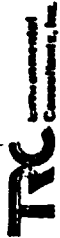
Nmograph					
C Factor					
Pilot Coefficient	0.84				
Orifice ΔH_A	1.80				
Test Start Time	9:55				
Test Final Time	11:21				
Leak Test Start	0.002	CPM	5	"14	
Leak Test Final	0.002	CPM	5	"14	

[illegible]

H ₂ O Collected	ml
SG Condition	
SG Weight	gms
Total Volume Collected	ml

CO ₂	O ₂	CO	N ₂

COMMENTS:



TRC
Environmental
Consultants, Inc.

EPA Method 19

FIELD DATA SHEET

Firm Name Alway
Plant Location MS
Test Number T-3
Sampling Location Stack 2
TRC Project No. 1638
Date 11-14-90
Tester ASB

Orifice No. 0-8
Ambient Temp. 51 °F
Bar. Press. 30.14 "Hg
Probe Ident. No. 301
Filter Ident. No. —
Duct Area 20x20 ft²

Nozzle No. & Dia. — in.
Assumed Moisture 3
Test Duration 64 min.
Traverse Point Interval 4 min.
Probe Heater Setting 250 °F
Filter Temp. Setting — °F
Dry Gas Meter Y 1.01

Monograph C Factor —
Pitot Coefficient 1.84
Orifice ΔH_A 1.56
Test Start Time 11:11
Test Final Time 13:50
Leak Test Start 0.000 CFM
Leak Test Final 0.000 CFM

Port	Point	Time Min.	Velocity AP in H ₂ O	ΔH in H ₂ O	T_M in °F	T_M out °F	P _{Stack} in H ₂ O	T_{Stack} °F	Gas Sample Volume cu. ft.	P R O B E	Cyc. Angle	Heater Box Temp.	Temp. of Gas Leaving Condenser °F	Pump Vac. in Hg	Probe Temp. °F	O ₂ %	Orsat Flow Rate (1pm) (SCFH)	F.O. Temp. °F
1	1	6	250	186	44	48		783	48373				46	2.5	346			
2	2	7	255	186	50	47		793	48717				43	2.5	346			
3	3	8	260	186	50	47		795	49027				45	2.5	341			
4	4	10	210	186	51	49		799	49337				47	2.5	341			
2	1	10	265	186	51	50		805	49644				47	2.5	346			
3	2	10	275	186	51	50		805	49955				50	2.5	346			
4	3	24	260	186	52	50		809	50268				50	1.5	341			
2	1	30	250	186	52	51		809	50579				51	2.5	346			
2	2	30	260	186	52	51		809	50887				49	2.5	346			
3	3	40	240	186	52	51		807	51200				49	3.0	346			
4	4	44	240	186	52	51		806	51510				51	3.0	341			
4	1	48	250	186	53	54		807	51820				53	3.0	342			
2	2	50	240	186	53	52		806	52130				48	3.0	346			
Average		Σ-AP																

H₂O Collected 41.7 ml
SG Condition 10.7
SG Weight —
Total Volume Collected 41.7 ml

Orsat Bag Sample Triplicate Analysis, %

CO ₂	O ₂	CO	H ₂

COMMENTS:

123 TAC ENVIRONMENTAL CONSULTANTS ALGOSHON GAS TRANSMISSION COMPANY HANOVER NJ EMISSION COMPLIANCE PROGRAM

1114 01 02 03 04 05 06 07 08 09 10 11 12 13 14 15 16
 100 CO PPM OXYGEN PERCENT NH3 PPM CO2 PERCENT CO PPM TWC PPM CS3 TEMP STACK TEMP WELLS TEMP

16:06:00	7.8	17.2	86.7	2.5	-4.0	16.000	-1.7	PPEN F	87.3F
200	7.8	17.2	86.9	2.5	-2.6		-0.4	PPEN	86.7
300	7.9	16.0	52.2	1.9	-4.2		1.3	WORLD	86.1
16:08:00	7.7	17.2	87.0	2.5	-2.0	4.0000	-0.1	PPEN F	86.2F
200	7.7	17.2	86.6	2.5	-3.3		-0.1	PPEN	86.7
300	8.1	16.6	50.3	2.0	-4.2		1.2	WORLD	86.1
16:10:00	7.7	17.2	87.0	2.5	-6.0	36.000	0.0	PPEN F	87.2F
200	7.8	17.2	86.7	2.5	-4.0		-0.1	PPEN	86.7
300	8.4	16.6	49.8	2.0	-4.2		1.2	WORLD	86.1
16:12:00	7.9	17.2	87.5	2.5	-6.0	16.000	0.1	PPEN F	87.1F
200	7.7	17.2	87.4	2.5	-4.0		0.0	PPEN	87.0
300	8.6	16.4	52.7	2.1	-4.2		1.2	WORLD	86.1
16:14:00	7.6	17.2	87.2	2.5	-2.0	4.0000	0.0	PPEN F	86.9F
200	7.7	17.2	87.3	2.5	-4.2		0.0	PPEN	87.0
300	8.9	17.0	55.5	1.8	-4.2		1.2	WORLD	86.1
16:16:00	7.8	17.2	87.0	2.5	-4.0	36.000	0.0	PPEN F	87.1F
200	7.6	17.2	86.9	2.5	-4.3		0.0	PPEN	87.1
300	9.0	17.5	58.4	1.8	-4.2		1.1	WORLD	86.2
16:18:00	7.8	17.2	86.0	2.5	-4.0	16.000	0.1	PPEN F	87.5F
200	7.6	17.2	86.6	2.5	-3.7		0.0	PPEN	87.3
300	9.0	18.1	61.2	1.9	-4.2		1.1	WORLD	86.2
16:20:00	7.9	17.2	86.7	2.0	-4.0	16.000	0.6	PPEN F	87.7F
200	7.7	17.2	86.5	2.4	-3.8		0.1	PPEN	87.3
300	9.3	18.1	64.0	2.0	-4.2		1.1	WORLD	86.3

OUT OF STACK

16:22:00	4.0	20.5	9.0	1.7	-4.0	16.000	0.0	PPEN F	87.5F
200	1.7	19.9	49.5	0.8	-3.8		0.5	PPEN	87.6
300	9.4	18.1	64.3	2.0	-4.2		1.1	WORLD	86.3

CPM 2.0 PARY 2

16:24:00	7.8	17.2	84.5	2.5	-4.0	16.000	0.1	PPEN F	87.0F
200	4.4	18.9	53.4	1.5	-4.1		0.3	PPEN	87.3
300	9.7	17.9	67.1	2.1	-4.2		1.1	WORLD	86.3

TRC ENVIRONMENTAL CONSULTANTS				ALGONQUIN GAS TRANSMISSION COMPANY HANDOVER NJ EMISSION COMPLIANCE PROGRAM											
123	01	02	03	04	05	06	07	08	09	10	11	12	13	14	15
1114	PPM	PERCENT	PERCENT		PPM		PERCENT		PPM		PPM C3		STACK		WELS
100	PPM												TEMP		TEMP
200															
16:46:00	8.4	17.1	95.2		95.2		2.5		-2.0	4.0000	0.0		OPEN F		81.6F
200	8.4	17.1	94.3		94.3		2.5		-3.3		0.1		OPEN		81.6
300	7.6	17.3	83.6		83.6		2.4		-4.1		0.0		WORLD		86.4
16:48:00	7.9	17.2	97.2		97.2		2.5		-4.0	16.000	-0.1		OPEN F		81.2F
200	8.3	17.1	95.6		95.6		2.5		-3.4		0.0		OPEN		81.4
300	7.6	17.3	84.1		84.1		2.4		-4.1		0.0		WORLD		86.2
16:50:00	7.7	17.2	98.0		98.0		2.5		-2.0	4.0000	-0.3		OPEN F		80.9F
200	8.0	17.1	96.5		96.5		2.5		-3.6		0.0		OPEN		81.2
300	7.6	17.3	84.6		84.6		2.4		-4.0		0.0		WORLD		86.0
16:52:00	7.5	17.2	98.2		98.2		2.5		-6.0	36.000	-0.4		OPEN F		80.8F
200	7.4	17.2	98.2		98.2		2.5		-4.0		-0.3		OPEN		80.8
300	7.6	17.3	85.2		85.2		2.4		-4.1		0.0		WORLD		85.8
16:54:00	7.6	17.2	98.0		98.0		2.5		-4.0	16.000	-0.4		OPEN F		79.9F
200	7.5	17.2	98.2		98.2		2.5		-4.0		-0.4		OPEN		80.6
300	7.6	17.3	85.6		85.6		2.4		-4.0		0.0		WORLD		85.5
16:56:00	7.5	17.2	97.7		97.7		2.5		-4.0	16.000	-0.4		OPEN F		79.9F
200	7.6	17.2	98.0		98.0		2.5		-3.6		-0.4		OPEN		79.6
300	7.6	17.3	86.1		86.1		2.4		-4.0		0.0		WORLD		85.3
16:58:00	7.7	17.2	98.2		98.2		2.5		-4.0	16.000	-0.6		OPEN F		79.9F
200	7.6	17.2	98.0		98.0		2.5		-4.4		-0.5		OPEN		79.7
300	7.6	17.3	86.6		86.6		2.4		-4.0		0.0		WORLD		85.2
17:00:00	8.0	17.1	97.0		97.0		2.5		-4.0	16.000	-1.0		OPEN F		79.3F
200	7.7	17.1	97.9		97.9		2.5		-4.4		-0.5		OPEN		79.7
300	7.6	17.3	87.3		87.3		2.4		-4.0		0.0		WORLD		84.9
17:05:43	-0.3	0.0	0.7		0.7		0.2	SYSTEM	-4.0	16.000	-0.2		OPEN F		79.0F
200	-11.4	11.0	0.5		0.5		0.2	ZERO	-4.0		-0.7		OPEN		79.1
300	7.1	16.2	82.4		82.4		2.3		-4.0		0.0		WORLD		84.5
17:17:54	-0.3	0.7	150.3		150.3		0.2		-4.0	16.000	-0.4		OPEN F		78.5F
200	-0.1	12.1	83.4		83.4		0.2		-3.8		-0.4		OPEN		78.3
300	5.5	13.4	82.8		82.8		1.8		-3.9		0.0		WORLD		82.8

TEST COMPLETE

ENVIRONMENTAL CONSUMABLES				HELIUM GAS TRANSMITTER COMPANY				HANDOVER NO EMISSION CHALLENGE PROGRAM										
125	1114	100	200	01	02	03	04	05	06	07	08	09	10	11	12	13	14	15
				CO	CO	OXYGEN	PERCENT	NOX	PPM	CO2	PERCENT	CO	PPM	THC	PPM	STACK	TEMP	HELS
17:21:42	300	300	300	-0.1	4.9	12.4	12.4	23.0	87.9	0.3	1.7	-4.0	16.000	-1.0	-1.0	PPEN F	76.8F	77.3
								23.0		0.3		-3.9		-0.1		PPEN	82.2	
								23.0		1.7						PPEN		
17:24:40	200	300	300	-1.3	4.5	12.4	12.4	0.5	87.9	12.0	1.9	-4.0	16.000	-0.6	-0.6	PPEN F	77.1F	77.7
								23.2		1.9		-3.4		-0.9		PPEN	81.5	
								24.8				-3.8		-0.2		PPEN		
17:27:52	200	300	300	-1.3	4.5	12.4	12.4	0.5	87.9	0.7	1.9	-4.0	16.000	-1.5	-1.5	PPEN F	76.2F	76.7
								23.2		1.9		-3.6		-0.6		PPEN	81.2	
								24.8		1.9		-3.8		-0.2		PPEN		
17:31:46	200	300	300	-0.1	4.2	12.4	12.4	-0.7	87.9	0.2	1.9	-4.0	16.000	-0.1	-0.1	PPEN F	75.9F	76.5
								23.0		1.9		-4.0		-0.1		PPEN	80.5	
								24.8		1.9		-3.9				PPEN		
17:37:03	200	300	300	-0.3	3.5	12.4	12.4	-0.3	87.9	0.1	1.9	-2.0	4.0000	4.9	4.9	PPEN F	74.7F	75.3
								23.0		1.9		-3.5		0.5		PPEN	79.3	
								24.8		1.9		-3.7				PPEN		
17:39:27	200	300	300	-0.6	3.2	12.4	12.4	-0.1	87.9	0.1	1.9	-6.0	36.000	4.5	4.5	PPEN F	PPEN F	
								23.0		1.9		-3.3		4.8		PPEN	75.2	
								24.8		1.9		-3.6		0.7		PPEN	78.9	
17:45:30	200	300	300	-0.3	3.5	12.4	12.4	-0.1	87.9	0.1	1.9	-4.0	16.000	4.4	4.4	PPEN F	67.2F	67.1
								23.0		1.9		-3.3		4.3		PPEN	77.7	
								24.8		1.9		-3.6		1.1		PPEN		
17:47:07	200	300	300	-0.2	3.2	12.4	12.4	-0.1	87.9	0.1	1.9	-6.0	16.000	4.2	4.2	PPEN F	67.2F	67.1
								23.0		1.9		-3.3		4.2		PPEN	77.7	
								24.8		1.9		-3.6		1.1		PPEN		
17:50:10	200	300	300	-0.3	3.5	12.4	12.4	-0.1	87.9	0.1	1.9	-6.0	16.000	4.2	4.2	PPEN F	67.2F	67.1
								23.0		1.9		-3.3		4.2		PPEN	77.7	
								24.8		1.9		-3.6		1.1		PPEN		
17:51:50	200	300	300	-0.3	3.5	12.4	12.4	-0.1	87.9	0.1	1.9	-6.0	16.000	4.2	4.2	PPEN F	67.2F	67.1
								23.0		1.9		-3.3		4.2		PPEN	77.7	
								24.8		1.9		-3.6		1.1		PPEN		
17:53:10	200	300	300	-0.3	3.5	12.4	12.4	-0.1	87.9	0.1	1.9	-6.0	16.000	4.2	4.2	PPEN F	67.2F	67.1
								23.0		1.9		-3.3		4.2		PPEN	77.7	
								24.8		1.9		-3.6		1.1		PPEN		
17:54:10	200	300	300	-0.3	3.5	12.4	12.4	-0.1	87.9	0.1	1.9	-6.0	16.000	4.2	4.2	PPEN F	67.2F	67.1
								23.0		1.9		-3.3		4.2		PPEN	77.7	
								24.8		1.9		-3.6		1.1		PPEN		

123 TEC ENVIRONMENTAL CONSULTANTS AIR CONDITION GAS TRANSMISSION COMPANY HANOVER NJ EMISSION COMPLIANCE PROGRAM

1114	01	02	03	04	05	06	07	08	09	10	11	12	13	14	15
100	01	02	03	04	05	06	07	08	09	10	11	12	13	14	15
200	01	02	03	04	05	06	07	08	09	10	11	12	13	14	15
	PPM	PPM	PERCENT	PPM	PPM	PPM	PERCENT	PERCENT	PPM	PPM	PPM	PPM	STACK	TEMP	WETS
17:53:14	-0.5		0.0		-1.0		5.4		-4.0	16.000	4.2		PPHEN		71.0F
200	-0.3		6.0		-0.6		5.1		-3.0		4.0		PPHEN		68.2
300	1.4		7.1		61.7		1.6		-3.6		1.6		MURID		75.8
17:55:28	40.9		0.0		-1.3		0.3		-4.0	16.000	4.0		PPHEN		73.5F
200	38.9		0.0		-1.1		0.3		-3.0		3.8		PPHEN		73.2
300	1.2		6.5		55.4		1.7		-3.6		1.8		MURID		75.5
17:56:54	9.5		0.7		-1.3		0.2		-4.0	16.000	4.2		PPHEN		72.5F
200	77.3		1.4		-1.1		0.2		-3.6		3.9		PPHEN		72.6
300	2.0		6.0		55.1		1.6		-3.6		1.9		MURID		75.2
18:00:36	0.9		21.6		-1.0		0.2		-2.0	4.0000	0.1		PPHEN		71.0F
200	1.1		21.6		-1.0		0.2		-3.3		0.6		PPHEN		72.7
300	1.7		5.7		48.5		1.5		-3.6		2.2		MURID		74.8
18:03:19	0.8		21.6		-1.0		0.2		-4.0	16.000	4.0		PPHEN		64.4F
200	1.0		21.6		-1.0		0.2		-3.2		3.8		PPHEN		67.4
300	1.7		6.3		47.7		1.5		-3.5		2.2		MURID		74.3
18:04:59	0.7		21.6		-1.0		0.2		-4.0	16.000	5.2		PPHEN		67.5F
200	1.0		21.6		-1.0		0.2		-3.2		3.8		PPHEN		67.4
300	1.9		7.0		47.6		1.5		-3.5		2.3		MURID		73.8

RACK

MID

RACK

SPAN

RACK

MID

ANALYZER

ZERO

ANALYZER

SPAN

ANALYZER

MID

APPENDIX B
Calibration and Certification Data

METHOD 5 MODULE CALIBRATION

DATE 11/20/90 ORIFICE/MODULE NO. D-8 NAME R. POTTER
 BAROMETRIC PRESSURE Pb 30.05 In Hg STANDARD METER P-687

MODULE ORIFICE SETTING ΔH (in. H ₂ O)	STANDARD METER			MODULE METER				γ	ΔH_a (in. H ₂ O)	Module Flowrate Q (SCFH)	OF
	Volume V_s (ft ³)	Factor Y_s	Temperature t_s (°F)	Pressure ΔP_s (in. H ₂ O)	Volume V_m (ft ³)	Temperatures t_m (°F)	Time θ (min)				
0.5	5.0	1.00	72	0.3	5.04	78	12.80	1.00	1.84		
1.5	5.0	1	72	0.3	5.04	78	9.21	1.00	1.84		
2.0	10.0	1	72	0.7	10.00	78	14.01	1.00	1.84		
3.0	10.0	1	72	0.8	10.00	78	12.88	1.00	1.84		
	10.0		72	1.3	10.00	78	10.34	1.00	1.84		
AVERAGE								1.00	1.84		

CHECK: ☐

FOR CHECK, USE THE AVERAGE ΔH_a FOR ΔH

$$Y = V_s (P_b + P_s) (T_m + 460) Y_s$$

$$V_m (P_b + \frac{\Delta H}{13.6}) (t_s + 460)$$

$$\Delta H_a = \left[\frac{(0.0317) \Delta H}{P_b (t_m + 460)} \right] \left[\frac{(t_s + 460) \theta}{V_s Y_s} \right]^2$$

$$Q = Y (17.64) V_m \left[\frac{P_b + \Delta H}{13.6} \right] \left[\frac{(t_m + 460) \theta}{(t_s + 460) \theta} \right]$$

$$OF = \text{orifice factor} = \left[\frac{(t_m + 460) \Delta H}{P_b} \right]^{1/2}$$

ACCEPTANCE CRITERIA:

Each Y must be 1.00 ± 0.01
 Average ΔH_a must be 1.84 ± 0.25
 Each ΔH_a must be within 0.15 of the average ΔH_a

$$Q = m (OF) + b$$

$$Q = \text{OF} +$$

TC Reconnect Calibrated with Constant Voltage Source OF
 tml or two Reference Thermometer OF
 Module Leak Check Probe Heater Low Control
 Heater Box Low Control OK Probe Heater Low Control
 Module Cleaned Pitot tube manometer leak check

Calibrated and Checked by R. Potter Date 11/20/90
 Reviewed by

PART 1 - PROBE CONFIGURATION

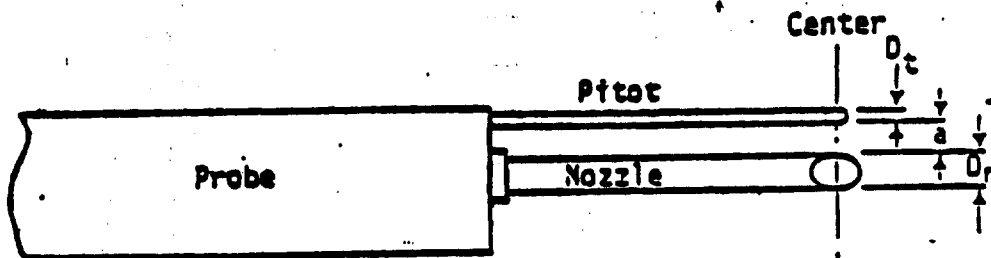
Date December 9, 1980
Page 01 of 01

TAC Probe Identification 302

Pitot Identification

Technical Specialist

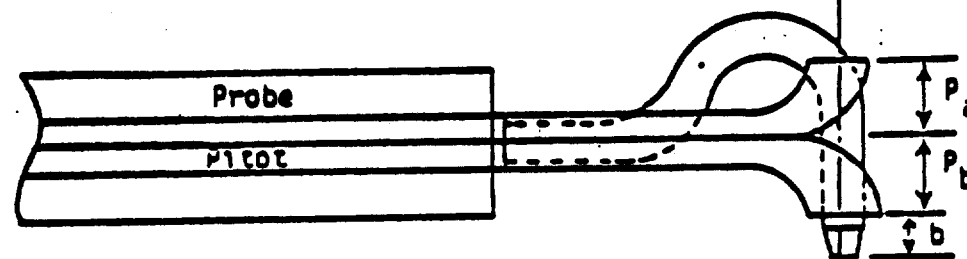
Date 11-01-90



D_t .375

D_n .507

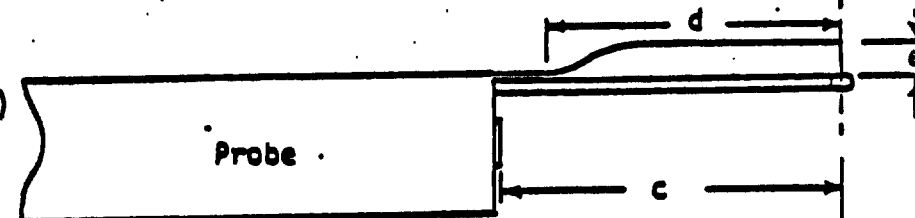
a .432



P_a .580

P_b .582

b 1.390

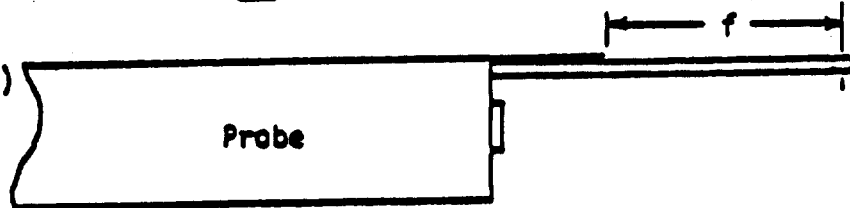


c 4.925

d 5.225

e .114

OR



c

f

Specifications (EPA Method 2)

$D_t = 3/16"$ to $3/8"$

$D_n = 1/2"$

$a \geq 3/4"$

$b \geq 0$

$c \geq 3"$

$d \geq 3"$

$e \geq 3/4"$

$f \geq 2"$

$P_a = P_b$

$1.05 D_t \leq P \leq 1.50 D_t$

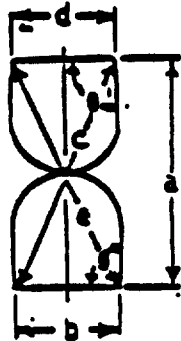
If these specifications are met, proceed with Part 2 Pitot alignment.

S-TYPE PITOT GEOMETRIC CALIBRATION
PART 2 - PITOT ALIGNMENT

TRC Probe Identification 302 Pitot Identification
 Technical Specialist
 Date 11-01-90

A.

Transverse
Tube Axis



a 1.119
 b .371
 c 1.151
 d .370
 e 1.164
 theta 85.51
 theta' 87.63

$$\frac{a^2 + b^2 - c^2}{2ab} = \cos \theta$$

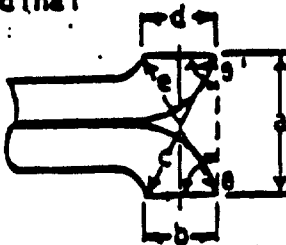
$$\frac{a^2 + d^2 - e^2}{2ad} = \cos \theta'$$

$$(80^\circ < \theta < 100^\circ)$$

$$(80^\circ < \theta' < 100^\circ)$$

B.

Longitudinal
Tube Axis



a 1.119
 b .521
 c 1.234
 d .523
 e 1.213
 theta 89.96
 theta' 87.34

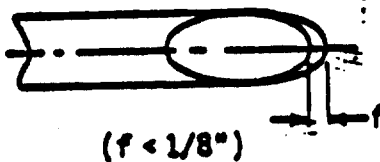
$$\frac{a^2 + b^2 - c^2}{2ab} = \cos \theta$$

$$\frac{a^2 + d^2 - e^2}{2ad} = \cos \theta'$$

$$(85^\circ < \theta < 95^\circ)$$

$$(85^\circ < \theta' < 95^\circ)$$

C.



(f < 1/8")

f < 1/8

D.



(g < 1/32")

g < 1/32

NOTE: values in parentheses are EPA Method 2 specifications.

PROBE THERMOCOUPLE CALIBRATION

Tolerances

Expected Stack Temperature (T_s) °R

Mercury Thermometer (T_{ref}) 786 °R

Thermocouple Readout 780 °R

Probe Identification 302

Technician AXS

(T_s ± 10%)

(T_{ref} ± 1.5%)

Date 11-6-90

PART 1 - PROBE CONFIGURATION

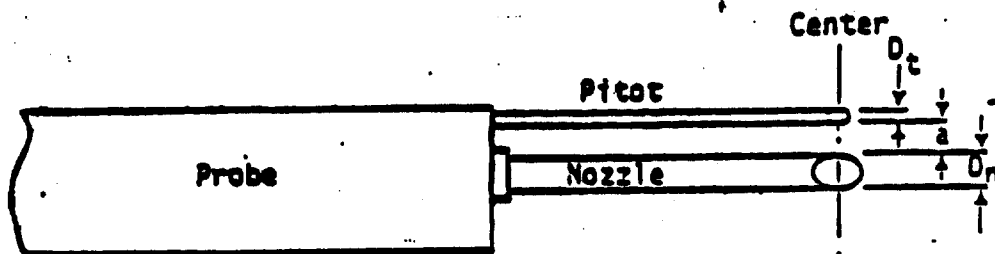
Date December 9, 1980
Page of

RC Probe Identification 301

Pitot Identification

Technical Specialist

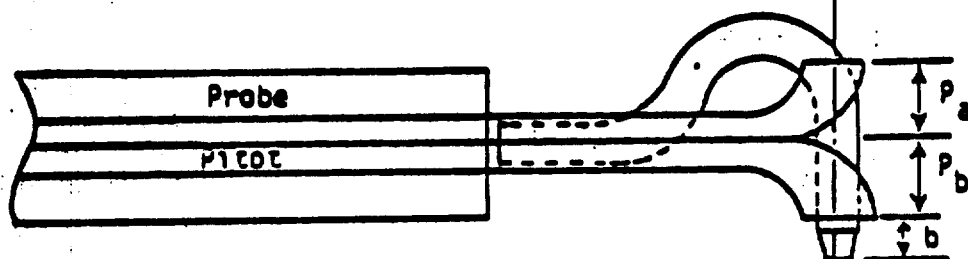
Date 10-01-90



D_t .380

D_n .507

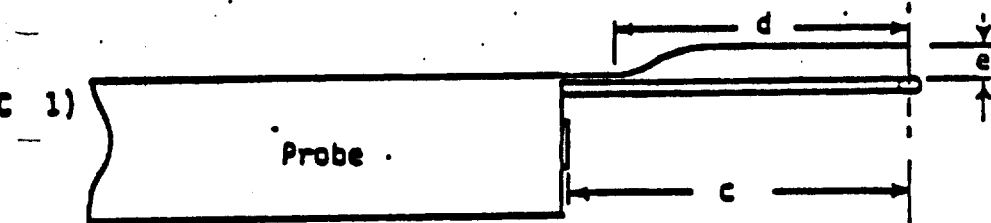
a .450



P_a .542

P_b .543

b 1.08



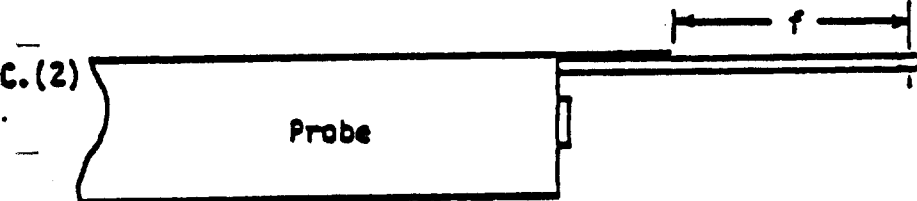
c 4.81

d 3.992

e .762

OR

OR



c

f

Specifications (EPA Method 2)

$D_t = 3/16"$ to $3/8"$

$D_n = 1/2"$

$a \geq 3/4"$

$b \geq 0$

$c \geq 3"$

$d \geq 3"$

$e \geq 3/4"$

$f \geq 2"$

$P_a = P_b$

$1.05 D_t \leq P \leq 1.50 D_t$

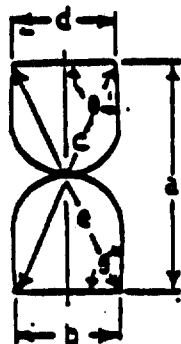
If these specifications are met, proceed with Part 2 Pitot alignment.

S-TYPE PITOT GEOMETRIC CALIBRATION
PART 2 - PITOT ALIGNMENT

TRC Probe Identification 301 Pitot Identification
 Technical Specialist
 Date 11/01/90

A.

Transverse
Tube Axis



a 1.094
 b .382
 c 1.152
 d .378
 e 1.153
 θ 88.93
 θ' 89.28

$$\frac{a^2 + b^2 - c^2}{2ab} = \cos \theta$$

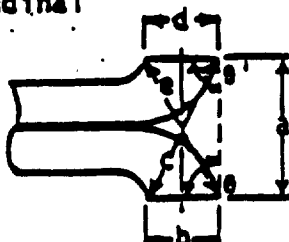
$$\frac{a^2 + d^2 - e^2}{2ad} = \cos \theta'$$

$$(80^\circ < \theta < 100^\circ)$$

$$(80^\circ < \theta' < 100^\circ)$$

B.

Longitudinal
Tube Axis



a 1.090
 b .301 .511
 c .249 1.237
 d .535
 e 1.197
 θ 94.17
 θ' 87.96

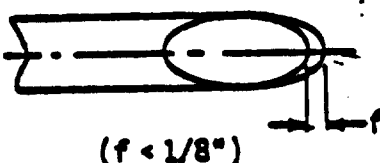
$$\frac{a^2 + b^2 - c^2}{2ab} = \cos \theta$$

$$\frac{a^2 + d^2 - e^2}{2ad} = \cos \theta'$$

$$(85^\circ < \theta < 95^\circ)$$

$$(85^\circ < \theta' < 95^\circ)$$

C.



(f < 1/8")

f < 1/8

D.



(g < 1/32")

g < 1/32

NOTE: values in parentheses are EPA Method 2 specifications.

PROBE THERMOCOUPLE CALIBRATION

Tolerances

Expected Stack Temperature (T_s) °R

Mercury Thermometer (T_{ref}) 660 °R

Thermocouple Readout 662 °R

Probe Identification 301

Technician ASB

Date 11-6-90

(T_s ± 10%)

(T_{ref} ± 1.5%)

F209

2L-1196

FORM
WATW

Scott Specialty Gases



Electronics Group

CERTIFICATION

ALL VALUES MOLE PERCENT UNLESS NOTED

GAS	REQUESTED	ACTUAL
CARBON MONOXIDE	9. PPM	10.1 PPM
NITROGEN	BALANCE	

REFERENCE		9.90 PPM
STANDARD	CWM 1677	AL 9208

ASSAY WAS PERFORMED	ACC.
TO EPA PROTOCOL 1	SEC G1

ANALYSIS DATE	6/20/89
---------------	---------

THC AS
METHANE _____ PPM

DEWPOINT _____ °F

PRESSURE 2000 PSIG

ANALYST MAB

EXPIRATION 12/20/90

F 259

2L - 1125



Scott Specialty Gases

Electronics Group

CERTIFICATION

ALL VALUES MOLE PERCENT UNLESS NOTED

GAS	REQUESTED	ACTUAL
CARBON MONOXIDE	<u>40. PPM</u>	<u>41.6 PPM</u>
NITROGEN	<u>BALANCE</u>	<u></u>
REFERENCE STANDARD	<u>CRM 678A</u>	<u>47.2 PPM</u> <u>CAL 6906</u>

ANALYSIS WAS PERFORMED ACC.
TO EPA PROTOCOL 1 SEC 61

ANALYSIS DATE 6/21/89

THC AS METHANE, _____ PPM

DEWPOINT _____ °F

PRESSURE 2000 PSI g

ANALYST MLB

EXPIRATION 12/21/90



Environmental
Consultants, Inc.

Part 2

EPA Method 19

FIELD DATA SHEET

Firm Name Allen & Co.
Plant Location NC
Test Number 7-3
Sampling Location Point 2
TRC Project No. 7638
Date 11/14/90
Tester ATB

Orifice No. D8
Ambient Temp. 30.4 °F
Bar. Press. 30.14 "Hg
Probe Ident. No. 203
Filter Ident. No. —
Duct Area 20" x 20" ft²

Nozzle No. & Dia. — in.
Assumed Moisture 3
Test Duration 64 min.
Traverse Point Interval 4 min.
Probe Heater Setting 250 °F
Filter Temp. Setting — °F
Dry Gas Meter Y 1.01

Monograph C Factor —
Pitot Coefficient 0.84
Orifice ΔH 1.80
Test Start Time 1222
Test Final Time 1350
Leak Test Start 0.002 CPME
Leak Test Final 0.002 CPME

Port	Point	Time Min.	Velocity AP in H ₂ O	ΔH in H ₂ O	T_M in °F	T_M out °F	P_{Stack} in H ₂ O	T_{Stack} °F	Gas Sample Volume cu. ft.	P R O B E	Cyc. Angle	Heater Box Temp.	Temp. of Gas Leaving Condenser °F	Pump Vac. in Hg	Probe Temp. °F	O ₂ i	Orsat Flow Rate (1pm) (SCFH)	F.O. Temp °F
	3	56	220	186	53	52	160	405	527	44			80	3.0	346			
	4	64	210	186	53	52		806	530	57			51	3.0	343			
		67							533	67								
Average		56	215	186	51	51	140	807	49.94									

Orsat Bag Sample
Triplicate Analysis.1

CO ₂	O ₂	CO	H ₂

H₂O Collected ml
SG Condition —
SG Weight —
Total Volume Collected ml

COMMENTS:

11/13/90

Algonquin Gas Co.

TURBINE # 1

TESTS 1-2

Long

123 100 200 08:59:47 09:07:18 03:21:46 08:31:15 08:47:30 09:02:48 08:08:29 08:10:39 08:14:21 08:16:42

TIME	CO	CO2	NOX	OXYGEN	TEMP	STACK	MELS
100	0.2	0.2	0.0	21.2	0.7	0.3	81.4
200	0.3	0.1	0.0	21.2	0.3	0.3	81.4
300	-0.7	0.1	-1.3	21.1	3.1	0.7	81.0
09:07:18	0.1	0.1	0.0	20.5	0.7	0.3	82.3F
200	-0.1	0.1	0.0	20.5	0.8	0.3	81.1
300	-0.5	0.1	-1.1	20.5	2.5	0.7	81.1
03:21:46	0.0	0.1	143.5	0.0	1.1	0.7	81.8F
200	0.0	0.1	143.5	0.0	1.2	0.7	80.9
300	-0.3	0.1	21.6	15.5	1.4	0.7	80.9
08:31:15	2.7	0.1	144.5	0.0	1.2	0.7	80.5F
200	0.0	0.1	142.2	0.0	1.2	0.7	81.7
300	0.0	0.1	50.3	12.1	0.7	0.7	80.7
08:47:30	0.1	0.1	147.5	0.0	1.2	0.7	79.1F
200	0.6	0.1	147.7	0.0	1.0	0.7	78.5
300	0.1	0.1	101.7	6.4	0.5	0.7	80.9
09:02:48	0.2	0.1	72.2	0.0	1.0	0.7	81.3F
200	3.1	0.1	72.4	0.0	0.0	0.7	81.4
300	0.6	0.1	139.7	3.8	0.7	0.7	80.9
08:08:29	0.0	0.1	0.2	0.0	1.9	0.7	81.1F
200	0.0	0.1	0.9	0.0	1.2	0.7	81.3
300	0.0	0.1	144.6	2.6	0.7	0.7	81.3
08:10:39	0.7	0.1	0.0	22.4	1.3	0.7	82.4F
200	0.0	0.1	0.4	14.8	0.7	0.7	81.8
300	0.0	0.1	144.6	3.3	0.7	0.7	80.8
08:14:21	-0.6	0.1	0.0	0.0	2.2	0.7	82.9F
200	-0.4	0.1	0.0	2.6	1.7	0.7	82.8
300	0.0	0.1	136.2	4.1	0.7	0.7	82.8
08:16:42	-1.3	0.1	0.2	0.2	2.6	0.7	82.4F
200	-0.7	0.1	0.1	1.6	0.8	0.7	82.7
300	0.0	0.1	131.6	4.2	0.8	0.7	81.0

CO2 570

CO2 570

11.70 MID RACK

22.70 SPAN

CO2 570

CO2 570

123	TRC ENVIRONMENTAL CONSULTANTS	01	02	03	04	05	06	07	08	09	10	11	12	13	14	15	16
100	CO PPM	O2 PERCENT	NOX PPM	SO2 PERCENT	CO2 PERCENT	CO PPM	CO PPM	CO PPM	CO PPM	CO PPM	CO PPM	CO PPM	CO PPM	CO PPM	CO PPM	CO PPM	CO PPM
09:31:43	41.5	0.0	0.2	0.1	0.1	-4.0	16.000	1.7	OPEN F	80.8F							
200	31.2	0.0	0.1	0.1	0.1	-2.2		1.1	OPEN	81.0							
300	2.9	4.1	94.0	1.1	1.1	-2.9		1.1	WORLD								
09:36:45	7.4	0.0	0.2	0.1	0.1	-2.0	4.0000	5.5	OPEN F	83.5F							
200	14.8	0.5	0.1	0.1	0.1	-2.6		3.1	OPEN	87.5							
300	4.7	4.1	72.8	1.1	1.1	-2.8		1.7	WORLD	81.2							
09:47:45	-0.3	0.0	146.0	0.1	0.1	-2.0	4.0000	3.8	OPEN F	78.6F							
200	0.0	0.0	145.2	0.1	0.1	-3.5		4.3	OPEN	78.9							
300	4.8	4.1	48.9	1.1	1.1	-2.8		1.7	WORLD	81.1							
09:50:23	-0.4	0.0	215.7	0.1	0.1	-2.0	4.0000	2.9	OPEN F	78.3F							
200	-0.1	0.0	170.8	0.1	0.1	-3.0		3.2	OPEN	78.2							
300	4.8	4.1	47.5	1.1	1.1	-2.2		1.8	WORLD	81.0							
09:50:48	-0.4	0.0	217.7	0.1	0.1	-2.0	4.0000	2.7	OPEN F	78.9F							
200	-0.1	0.0	173.0	0.1	0.1	-3.0		3.2	OPEN	78.3							
300	4.8	4.1	47.5	1.1	1.1	-2.8		1.8	WORLD	81.0							
09:53:45	8.2	0.0	3.0	0.1	0.1	-4.0	16.000	3.5	OPEN F	79.1F							
200	7.5	0.0	94.7	0.1	0.1	-3.2		1.8	OPEN	79.6							
300	4.8	4.1	47.6	1.1	1.1	-2.8		1.8	WORLD	81.0							
09:55:21	41.5	0.0	0.2	0.1	0.1	-4.0	16.000	2.8	OPEN F	78.7F							
200	13.5	0.0	48.0	0.1	0.1	-3.3		2.4	OPEN	79.4							
300	5.1	3.7	40.6	1.0	1.0	-2.9		1.9	WORLD	81.0							
09:58:15	0.1	0.2	71.7	0.1	0.1	-2.0	4.0000	1.4	OPEN F	78.5F							
200	0.1	0.4	64.6	0.1	0.1	-2.8		0.0	OPEN	79.2							
300	6.5	2.3	35.1	1.0	1.0	-2.8		1.9	WORLD	80.9							
10:05:14	0.2	0.0	72.5	0.1	0.1	-4.0	4.0000	0.1	OPEN F	80.0F							
200	0.0	0.0	73.2	0.1	0.1	-3.2		0.9	OPEN	80.0							
300	6.5	2.1	37.6	1.0	1.0</												

173	TRC ENVIRONMENTAL CONSULTANTS	ALGONQUIN	URS TRANSMISSION	COMP	03	07	CD2	PERCENT	CO	PPM	THC	PPM C3	STACK	TEMP	15	16
100	01	02	03	04	05	06	07	08	09	10	11	12	13	14	15	16
200	CO	OXYGEN	NOX	NOX	NOX	CO2	PERCENT	CO	PPM	THC	PPM C3	OPEN F	OPEN F	TEMP	TEMP	TEMP
300	PPM	PERCENT	PPM	PPM	PPM	PERCENT	PERCENT	PPM	PPM	PPM	PPM	PPM	PPM	PPM	PPM	PPM
10:10:58	0.0	0.0	72.7	72.7	72.7	0.1	0.1	-2.0	4.0000	4.8	4.8	PPM	PPM F	78.1F	78.1F	78.1F
10:10:58	0.0	0.0	73.4	73.4	73.4	0.1	0.1	-2.6		13.8	13.8	PPM	PPM F	78.5	78.5	78.5
10:10:58	6.5	0.9	42.5	42.5	42.5	1.0	1.0	-2.9		2.2	2.2	PPM	PPM F	80.3	80.3	80.3
10:48:23	-0.8	0.0	134.7	134.7	134.7	0.1	0.1	-4.0	16.000	-0.1	-0.1	PPM	PPM F	75.1F	75.1F	75.1F
10:48:23	-0.7	0.0	133.7	133.7	133.7	0.1	0.1	-3.7		-0.1	-0.1	PPM	PPM F	79.8	79.8	79.8
10:48:23	1.1	4.0	90.6	90.6	90.6	0.1	0.1	-3.1		0.7	0.7	PPM	PPM F	80.7	80.7	80.7
10:49:01	-0.5	0.0	136.3	136.3	136.3	0.1	0.1	-4.0	16.000	-0.2	-0.2	PPM	PPM F	76.5F	76.5F	76.5F
10:49:01	-0.7	0.0	134.3	134.3	134.3	0.1	0.1	-3.8		-0.1	-0.1	PPM	PPM F	78.4	78.4	78.4
10:49:01	1.1	4.0	90.6	90.6	90.6	0.1	0.1	-3.1		0.7	0.7	PPM	PPM F	80.7	80.7	80.7
10:49:33	-0.9	0.0	137.2	137.2	137.2	0.1	0.1	-4.0	16.000	-0.2	-0.2	PPM	PPM F	78.7F	78.7F	78.7F
10:49:33	-0.7	0.0	134.3	134.3	134.3	0.1	0.1	-3.8		-0.1	-0.1	PPM	PPM F	78.3	78.3	78.3
10:49:33	1.1	4.0	90.6	90.6	90.6	0.1	0.1	-3.1		0.7	0.7	PPM	PPM F	80.7	80.7	80.7
10:52:03	-1.3	0.0	82.3	82.3	82.3	0.5	0.5	-4.8	16.000	-0.3	-0.3	PPM	PPM F	73.8F	73.8F	73.8F
10:52:03	0.9	4.0	82.3	82.3	82.3	0.5	0.5	-3.2		0.6	0.6	PPM	PPM F	73.7	73.7	73.7
10:56:22	35.9	1.5	82.3	82.3	82.3	0.5	0.5	-4.0	16.000	-0.3	-0.3	PPM	PPM F	80.3F	80.3F	80.3F
10:56:22	19.1	0.4	82.2	82.2	82.2	0.6	0.6	-3.9		0.4	0.4	PPM	PPM F	80.7	80.7	80.7
10:56:22	1.1	4.0	82.2	82.2	82.2	0.6	0.6	-3.2		0.4	0.4	PPM	PPM F	80.7	80.7	80.7
11:00:05	2.1	2.9	82.2	82.2	82.2	0.6	0.6	-4.0	16.000	-0.3	-0.3	PPM	PPM F	79.9F	79.9F	79.9F
11:00:05	1.8	4.2	82.2	82.2	82.2	0.6	0.6	-3.3		0.3	0.3	PPM	PPM F	80.1	80.1	80.1
11:00:05	1.8	4.2	82.2	82.2	82.2	0.6	0.6	-3.3		0.3	0.3	PPM	PPM F	80.8	80.8	80.8
11:14:00	13.9	17.6	82.2	82.2	82.2	0.6	0.6	-4.0	16.000	2.2	2.2	PPM	PPM F	77.1F	77.1F	77.1F
11:14:00	13.9	17.5	82.2	82.2	82.2	0.6	0.6	-4.0		2.7	2.7	PPM	PPM F	78.0	78.0	78.0
11:14:00	2.7	8.0	82.2	82.2	82.2	0.6	0.6	-3.5		0.3	0.3	PPM	PPM F	80.5	80.5	80.5
11:16:00	13.0	17.5	82.2	82.2	82.2	0.6	0.6	-4.0	16.000	1.7	1.7	PPM	PPM F	76.6F	76.6F	76.6F
11:16:00	13.3	17.5	82.2	82.2	82.2	0.6	0.6	-4.0		1.9	1.9	PPM	PPM F	76.7	76.7	76.7
11:16:00	3.2	7.9	82.2	82.2	82.2	0.6	0.6	-3.6		0.4	0.4	PPM	PPM F	80.4	80.4	80.4
11:18:00	12.6	17.3	82.2	82.2	82.2	0.6	0.6	-4.8	16.000	1.6	1.6	PPM	PPM F	74.3F	74.3F	74.3F
11:18:00	12.6	17.3	82.2	82.2	82.2	0.6	0.6	-3.6		0.4	0.4	PPM	PPM F	80.1	80.1	80.1
11:18:00	3.6	8.4	82.2	82.2	82.2	0.6	0.6	-3.6		0.4	0.4	PPM	PPM F	80.1	80.1	80.1

123	1113	100	200	11:20:00	200	300	11:22:00	200	300	11:24:00	200	300	11:26:00	200	300	11:28:00	200	300	11:30:00	200	300	11:32:00	200	300	11:34:00	200	300	11:36:00	200	300	11:38:00	200	300																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																											
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CD			OXYGEN			NOX			CO2			PPM			THC			PPM C3			STACK			TEMP			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F			OPEN F		

TEST 1 11/13/90 11:30 START

123
1113
100
200
12:20:00
200
300
12:22:00
200
300
12:24:00
200
300
12:26:00
200
300
12:28:00
200
300
12:30:00
200
300
12:32:00
200
300
12:34:00
200
300
12:36:00
200
300
12:38:00
200
300

TEMP EQUIPMENTAL ANALYSIS TAUTS
04
03
02
01
CO
PPM

05
04
03
02
NOX
PPM

06
05
04
03
GAS
PERCENT

07
06
05
04
CO2
PERCENT

08
07
06
05
CO
PPM

09
08
07
06
PPH
PPM

10
09
08
07
PPH
PPM

11
10
09
08
TMC
PPH

12
11
10
09
PPH
PPH

13
12
11
10
STACK
TEMP

14
13
12
11
STACK
TEMP

15
14
13
12
MELT
TEMP

16
15
14
13
MELT
TEMP

17
16
15
14
MELT
TEMP

18
17
16
15
MELT
TEMP

19
18
17
16
MELT
TEMP

20
19
18
17
MELT
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123	1	TR	PIRT	UTAL	ISUL	S	DNOL	IRS	ISMT	M	CI	NV	H	HER	10	MIS	TIME	ICF	13	14	15
1113		N1	N2	N3	N4		N5	N6	N7		N8	N9							STCK		
100		CM		PERCENT			PPH		CM2			CM				PPH	THC		TEMP		
200		PPH							PERCENT			PPH					CM3				
14:26:00		10.1		17.2			79.2		2.4			-4.0		16.000		8.0		OPEN F		76.20	
200		11.2		17.2			78.7		2.4			-3.8				9.6		OPEN		77.1	
300		26.1		19.0			41.7		1.3			-4.1				12.2		MURID		79.7	
14:28:00		8.5		17.2			81.0		2.3			-4.0		16.000		6.0		OPEN F		75.66	
200		10.2		17.2			79.4		2.3			-3.6				8.2		OPEN		76.9	
300		26.4		18.9			44.4		1.4			-4.1				12.4		MURID		79.6	
14:30:00		8.0		17.3			80.2		2.3			-4.0		16.000		4.6		OPEN F		75.96	
200		7.8		17.3			80.6		1.2.3			-3.3				4.9		OPEN		75.0	
300		26.7		18.7			47.1		1.5			-4.1				12.5		MURID		79.5	
14:32:00		6.9		17.4			80.2		2.2			-4.0		16.000		3.7		OPEN F		75.56	
200		7.3		17.3			80.4		2.2			-3.7				4.3		OPEN		75.5	
300		27.0		18.6			49.2		1.5			-4.1				12.6		MURID		79.4	
14:34:00		5.6		17.4			77.0		2.2			-4.0		16.000		3.1		OPEN F		73.86	
200		7.0		17.3			79.6		2.2			-3.8				3.9		OPEN		75.0	
300		27.2		18.5			52.3		1.6			-4.1				12.4		MURID		79.3	
14:36:00		6.7		17.5			74.7		2.1			-2.0		4.0000		2.7		OPEN F		74.66	
200		6.7		17.4			76.1		2.1			-3.3				2.8		OPEN		74.9	
300		27.5		18.3			54.8		1.7			-4.0				12.2		MURID		79.1	
14:38:00		6.9		17.6			70.5		2.1			-2.0		4.0000		2.5		OPEN F		74.66	
200		6.8		17.5			74.4		2.1			-2.8				2.6		OPEN		74.4	
300		27.8		18.2			57.1		1.7			-4.0				12.3		MURID		78.9	
14:40:00		7.2		17.7			67.5		2.0			-2.0		4.0000		2.2		OPEN F		75.26	
200		7.2		17.6			67.9		2.0			-2.0				2.2		OPEN		74.8	
300		28.1		18.1			59.4		1.8			-3.9				12.4		MURID		78.8	
14:42:00		7.3		17.8			63.5		2.0			-2.0		4.0000		2.0		OPEN F		73.86	
200		7.2		17.2			66.1		2.0			-2.3				2.0		OPEN		74.6	
300		28.4		18.0			61.5		1.8			-3.8				12.4		MURID		78.6	
14:44:00		7.4		17.9			64.5		1.9			-3.9		16.000		3.6		OPEN F		74.96	
200		7.3		17.9			63.5		1.9			-3.8				12.5		OPEN		78.5	

123	1 TR	01	02	03	04	05	06	07	08	09	10	11	12	13	14	15	16
1113	TR	01	02	03	04	05	06	07	08	09	10	11	12	13	14	15	16
100	CD	PPM	OXYGEN	PPM	CD2	PPM	CD	PPM	THC	PPM	CD	PPM	CD	PPM	CD	PPM	CD
200	CD	PPM	OXYGEN	PPM	CD2	PPM	CD	PPM	THC	PPM	CD	PPM	CD	PPM	CD	PPM	CD
12:40:00	6.1	17.7	64.2	2.1	-4.0	16.000	0.4	OPEN F	80.6F								
200	6.0	17.7	64.3	2.0	-4.0		0.3	OPEN	80.6								
300	6.6	17.3	72.8	2.3	-3.8		0.3	DURLD	80.0								
12:42:00	5.5	17.7	63.2	2.1	-4.0	16.000	0.3	OPEN F	81.5F								
200	5.8	17.7	63.9	2.0	-3.8		0.3	OPEN	81.0								
300	6.5	17.3	72.3	2.2	-3.8		0.3	DURLD	80.0								
12:44:00	5.5	17.6	64.5	2.1	-4.0	16.000	0.2	OPEN F	81.6F								
200	5.7	17.6	63.7	2.0	-3.9		0.3	OPEN	81.3								
300	6.4	17.3	71.9	2.2	-3.8		0.3	DURLD	80.0								
12:46:00	5.7	17.6	66.0	2.2	-4.0	16.000	0.1	OPEN F	79.5F								
200	5.5	17.6	65.3	2.1	-4.0		0.2	OPEN	78.4								
300	6.4	17.3	71.6	2.2	-3.8		0.3	DURLD	80.0								
12:48:00	5.1	17.6	66.5	2.1	-4.0	16.000	0.3	OPEN F	80.2F								
200	5.5	17.6	65.8	2.1	-3.7		0.2	OPEN	78.9								
300	6.3	17.4	71.2	2.2	-3.8		0.3	DURLD	79.9								
12:53:56	-1.3	9.8	131.7	0.4	-3.5	16.000	0.3	OPEN F	83.1F								
200	1.3	7.8	96.7	0.8	-3.8		0.4	OPEN	80.1								
300	6.0	16.9	72.1	2.1	-3.8		0.4	DURLD	80.1								
12:54:16	-1.2	0.0	133.0	0.1	-4.0	16.000	0.3	OPEN F	83.6F								
200	-1.3	0.0	132.7	0.1	-2.0		0.4	OPEN	83.4								
300	5.7	16.3	73.9	2.0	-3.8		0.4	DURLD	80.1								
12:57:38	-1.3	-0.1	12.7	12.7	-4.0	16.000	0.3	OPEN F	83.4F								
200	-1.2	0.0	118.8	0.2	-2.9		0.2	OPEN	82.9								
300	5.4	15.7	75.7	2.0	-3.7		0.4	DURLD	80.1								
13:01:58	-1.2	0.0	74.5	0.3	-2.0	4.0000	0.1	OPEN F	70.2F								
200	-1.2	0.5	46.4	1.8	-2.3		0.2	OPEN	73.7								
300	4.8	14.6	71.7	2.3	-3.6		0.4	DURLD	80.0								
13:06:17	-1.2	27.1	0.2	0.1	-4.0	16.000	-0.8	OPEN F	74.5F								
200	-1.1	20.3	19.0	0.1	-2.6		-0.8	OPEN	70.8								
300	4.0	14.0	68.8	2.0	-3.6		0.3	DURLD	79.0								

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END

T-1-12.2

[illegible]

123 1113 100 200	TBC ENVIRONMENTAL CONSULTANTS			AIR QUALITY GAS TRANSMISSION COMPANY NUMBER			EMISSIONS REPORT NUMBER			PR		
	01 CO PPM	02 EXHAUST PERCENT	03 PERCENT	04 N4	05 NMH PPM	06 PERCENT	07 PERCENT	08 PERCENT	09 PERCENT	10 PERCENT	11 PERCENT	12 PERCENT
15:06:00	6.0	18.7	18.7	35.7	35.7	1.6	1.6	1.6	1.6	16.000	0.9	0.9
200	6.1	18.6	18.6	36.9	36.9	1.6	1.6	1.6	1.6	16.000	0.9	0.9
300	25.5	17.8	17.8	60.5	60.5	1.9	1.9	1.9	1.9	16.000	0.9	0.9
15:08:00	6.0	18.7	18.7	33.5	33.5	1.6	1.6	1.6	1.6	16.000	0.9	0.9
200	6.0	18.6	18.6	35.5	35.5	1.6	1.6	1.6	1.6	16.000	0.9	0.9
300	21.7	17.9	17.9	58.9	58.9	1.9	1.9	1.9	1.9	16.000	0.9	0.9
15:10:00	6.0	18.7	18.7	33.8	33.8	1.6	1.6	1.6	1.6	16.000	0.9	0.9
200	6.0	18.7	18.7	33.6	33.6	1.6	1.6	1.6	1.6	16.000	0.9	0.9
300	17.9	17.9	17.9	57.5	57.5	1.9	1.9	1.9	1.9	16.000	0.9	0.9

SUR OF STACK 80M CEM STILL IN STACK

15:12:00 200 300	TBC ENVIRONMENTAL CONSULTANTS			AIR QUALITY GAS TRANSMISSION COMPANY NUMBER			EMISSIONS REPORT NUMBER			PR		
	01 CO PPM	02 EXHAUST PERCENT	03 PERCENT	04 N4	05 NMH PPM	06 PERCENT	07 PERCENT	08 PERCENT	09 PERCENT	10 PERCENT	11 PERCENT	12 PERCENT
15:12:00	5.9	18.7	18.7	33.8	33.8	1.6	1.6	1.6	1.6	16.000	0.9	0.9
200	5.9	18.7	18.7	33.7	33.7	1.6	1.6	1.6	1.6	16.000	0.9	0.9
300	14.1	18.0	18.0	56.0	56.0	1.9	1.9	1.9	1.9	16.000	0.9	0.9
15:14:00	6.1	18.6	18.6	33.8	33.8	1.6	1.6	1.6	1.6	16.000	0.9	0.9
200	5.9	18.6	18.6	33.8	33.8	1.6	1.6	1.6	1.6	16.000	0.9	0.9
300	10.4	18.0	18.0	54.6	54.6	1.9	1.9	1.9	1.9	16.000	0.9	0.9
15:16:00	7.1	18.4	18.4	38.2	38.2	1.7	1.7	1.7	1.7	16.000	0.7	0.7
200	6.7	18.5	18.5	35.8	35.8	1.6	1.6	1.6	1.6	16.000	0.7	0.7
300	8.5	18.1	18.1	53.4	53.4	1.8	1.8	1.8	1.8	16.000	0.7	0.7
15:18:00	7.2	18.4	18.4	38.2	38.2	1.7	1.7	1.7	1.7	16.000	0.7	0.7
200	6.9	18.4	18.4	37.0	37.0	1.6	1.6	1.6	1.6	16.000	0.7	0.7
300	7.6	18.1	18.1	52.2	52.2	1.8	1.8	1.8	1.8	16.000	0.7	0.7
15:20:00	7.3	18.4	18.4	37.7	37.7	1.7	1.7	1.7	1.7	16.000	0.7	0.7
200	7.2	18.4	18.4	37.7	37.7	1.7	1.7	1.7	1.7	16.000	0.7	0.7
300	7.0	18.1	18.1	51.0	51.0	1.8	1.8	1.8	1.8	16.000	0.7	0.7
15:22:00	6.8	18.4	18.4	37.2	37.2	1.7	1.7	1.7	1.7	16.000	0.7	0.7
200	7.1	18.4	18.4	37.5	37.5	1.7	1.7	1.7	1.7	16.000	0.7	0.7
300	6.7	18.2	18.2	49.9	49.9	1.8	1.8	1.8	1.8	16.000	0.7	0.7
15:24:00	6.9	18.4	18.4	35.7	35.7	1.7	1.7	1.7	1.7	16.000	0.7	0.7
200	6.9	18.4	18.4	35.7	35.7	1.7	1.7	1.7	1.7	16.000	0.7	0.7
300	6.5	18.2	18.2	48.4	48.4	1.9	1.9	1.9	1.9	16.000	0.7	0.7

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75.7F
75.5F

123 TAC ENVIRONMENTAL CONSULTANTS ALUMINUM GAS TRANSMISSION COMPANY HANOVER NJ EMISSION COMPLIANCE PROGRAM

1113	01	02	03	04	05	06	07	08	09	10	11	12	13	14	15	16
LOC	CON	PPM	NOXGEN	PERCENT	PPM	PPM	PERCENT	PPM	PPM	PPM	TWC	PPM	STACK	TEMP	WFLS	TEMP
200	6.8	18.6	35.2	1.7	-4.0	16.000	0.7	OPEN F	75.7F							
200	6.7	18.6	35.2	1.7	-4.0	16.000	0.5	OPEN F	75.7							
300	6.4	18.3	47.0	1.7	-3.4	16.000	1.6	OPEN F	75.5							
15:26:00	6.8	18.6	35.2	1.7	-4.0	16.000	0.9	OPEN F	77.1F							
200	6.7	18.6	35.2	1.7	-3.8	16.000	0.6	OPEN F	75.8							
300	6.3	18.3	45.4	1.7	-3.4	16.000	1.5	OPEN F	75.6							
15:30:00	6.6	18.6	35.2	1.7	-4.0	16.000	0.9	OPEN F	73.4F							
200	6.7	18.6	35.1	1.7	-3.6	16.000	0.8	OPEN F	74.2							
300	6.3	18.4	47.0	1.7	-3.4	16.000	1.3	OPEN F	75.5							
15:32:00	6.8	18.6	35.5	1.7	-2.0	4.0000	0.7	OPEN F	75.5F							
200	6.8	18.6	35.3	1.6	-3.5	4.0000	0.7	OPEN F	74.2							
300	6.3	18.4	47.5	1.7	-3.4	4.0000	1.2	OPEN F	75.5							
15:34:00	6.9	18.5	36.3	1.7	-4.0	16.000	0.6	OPEN F	75.9F							
200	6.9	18.5	35.6	1.6	-3.4	16.000	0.7	OPEN F	75.0							
300	6.3	18.4	41.1	1.6	-3.4	16.000	1.2	OPEN F	75.6							
15:36:00	30.6	19.0	20.5	1.4	-4.0	16.000	1.4	OPEN F	75.5F							
200	29.4	18.9	29.3	1.4	-3.6	16.000	1.4	OPEN F	75.3							
300	7.1	18.5	39.3	1.6	-3.4	16.000	1.1	OPEN F	75.6							
15:38:00	34.5	19.0	16.3	1.5	-4.0	16.000	1.5	OPEN F	75.5F							
200	31.9	18.9	21.2	1.4	-3.8	16.000	1.5	OPEN F	75.9							
300	8.0	18.5	37.5	1.6	-3.5	16.000	1.1	OPEN F	75.6							
15:40:00	33.5	19.0	15.7	1.0	-4.0	16.000	32.7	OPEN F	74.6F							
200	33.4	18.9	19.0	1.4	-4.0	16.000	10.9	OPEN F	76.0							
300	8.9	18.6	35.8	1.6	-3.6	16.000	2.1	OPEN F	75.6							
15:42:00	-0.9	21.1	2.0	0.2	-4.0	16.000	13.8	OPEN F	75.4F							
200	3.6	20.6	8.1	0.3	-4.0	16.000	20.9	OPEN F	74.8							
300	8.6	18.7	33.7	1.5	-3.6	16.000	2.5	OPEN F	75.7							
15:44:00	-1.3	21.1	0.5	0.2	-4.0	16.000	11.4	OPEN F	75.7F							
200	1.2	20.8	4.5	0.2	-3.9	16.000	15.2	OPEN F	75.1							
300	8.4	18.8	31.7	1.5	-3.6	16.000	2.8	OPEN F	75.7							

TEST 2 COMPLETE

[illegible]

TAC ENVIRONMENTAL CONSULTANTS				ALGONQUIN GAS TRANSMISSION COMPANY				HAMILTON, ONTARIO				EMISSION COMPLIANCE PROGRAM			
123	01	02	03	04	05	06	07	08	09	10	11	12	13		
1113	CO	PPM	OXYGEN	PERCENT	NOX	PPM	SO2	PERCENT	CO	PPM	THC	STACK	TEMP		
16:38:46	-0.9	21.4	-0.5	0.2	-2.0	4.0000	9.1	9.6	APEN F						
200	1.3	17.1	-0.4	0.1	-2.1				APEN						
300	3.5	10.9	14.3	0.3	-3.0				APEN F						
16:46:49	-1.7	0.8	15.5	0.1	-2.0	4.0000	0.5	0.5	APEN F						
200	2.3	9.9	19.4	0.3	-3.0				APEN						
300	7.3	7.9	28.6	0.3	-3.0				APEN F						
16:53:26	-1.3	0.2	0.0	0.1	-2.0	4.0000	0.4	0.4	APEN F						
200	1.2	11.3	41.6	0.1	-2.4				APEN						
300	2.3	7.9	28.6	0.3	-3.0				APEN F						
16:57:17	-1.3	0.2	0.0	0.1	-2.0	4.0000	0.4	0.4	APEN F						
200	1.2	11.3	41.6	0.1	-2.4				APEN						
300	2.3	7.9	28.6	0.3	-3.0				APEN F						
17:01:59	-1.3	0.2	0.0	0.1	-2.0	4.0000	0.4	0.4	APEN F						
200	1.2	11.3	41.6	0.1	-2.4				APEN						
300	2.3	7.9	28.6	0.3	-3.0				APEN F						
17:08:52	-1.3	0.2	0.0	0.1	-2.0	4.0000	0.4	0.4	APEN F						
200	1.2	11.3	41.6	0.1	-2.4				APEN						
300	2.3	7.9	28.6	0.3	-3.0				APEN F						
17:14:35	-1.3	0.2	0.0	0.1	-2.0	4.0000	0.4	0.4	APEN F						
200	1.2	11.3	41.6	0.1	-2.4				APEN						
300	2.3	7.9	28.6	0.3	-3.0				APEN F						
17:18:22	-1.3	0.2	0.0	0.1	-2.0	4.0000	0.4	0.4	APEN F						
200	1.2	11.3	41.6	0.1	-2.4				APEN						
300	2.3	7.9	28.6	0.3	-3.0				APEN F						

ALGONQUIN

UNIT 2

TESTS 1 2 3

UNIT 1

TEST 3

11/14/90

Front

TAC ENVIRONMENTAL CONSULTANTS ALGONQUIN GAS TRANSMISSION COMPANY HANOVER NJ EMISSION COMPLIANCE PROGRAM

123 1114 100 200 06:01:43 200 300 06:07:35 200 300 06:09:32 200 300 06:19:01 200 300 06:23:17 200 300 06:23:39 200 300 06:26:51 200 300 06:29:48 200 300 06:32:39 200 300 06:32:59 200 300

01	02	03	04	05	06	07	08	09	10	11	12	13	14	15	16
CO	PPM	OXYGEN	PERCENT	NOX	PPM	CO2	PERCENT	CO	PPM	THC	PPM C3	STACK	TEMP	MEIS	TEMP
41.5	SPAD	0.1		0.2		0.2		-4.0	16.000	-1.3		OPEN F		81.7F	
71.2		0.3		0.1		1.9		-4.0		-1.1		OPEN		81.4	
-0.3		11.5		25.6		1.2		-3.6		1.3		MURID		80.6	
9.2	MP	0.0		0.2		0.1		-4.0	16.000	-0.8		OPEN F		80.7F	
9.1		0.0		0.2		0.1		-4.0		-1.2		OPEN		80.6	
1.7		9.4		25.6		1.2		-3.6		1.2		MURID		80.6	
0.8		21.2		0.2		0.2		-4.0	16.000	-0.1		OPEN F		79.3F	
7.3		3.6		0.2		0.1		-3.9		-0.9		OPEN		80.4	
2.1		8.7		25.6		1.2		-3.6		1.1		MURID		80.5	

06:19:01	06:23:17	06:23:39	06:26:51	06:29:48	06:32:39	06:32:59
0.0	-0.2	-0.1	-0.1	-1.3	36.1	38.5
7.4	-0.1	-0.1	-0.1	-0.4	10.1	13.3
2.6	2.7	2.7	2.7	2.7	3.5	3.5
0.2	0.0	0.0	0.0	0.0	0.0	0.0
0.8	0.0	0.0	0.0	0.0	0.0	0.0
25.6	132.7	28.0	28.0	36.5	28.2	28.2
0.2	0.1	0.1	0.1	0.1	0.2	0.2
0.1	0.1	0.1	0.1	0.1	0.5	0.4
1.2	1.2	1.2	1.2	1.2	1.7	1.7
-4.0	-4.0	-4.0	-4.0	-4.0	-4.0	-4.0
-4.0	-4.0	-4.0	-4.0	-4.0	-4.0	-4.0
-3.8	-3.9	-3.9	-3.9	-3.9	-3.9	-3.9
16.000	16.000	16.000	16.000	16.000	16.000	16.000
-0.2	-0.1	-0.1	-0.1	-0.2	-0.2	-0.2
-0.2	-0.1	-0.1	-0.1	-0.2	-0.2	-0.2
1.4	1.4	1.4	1.4	1.3	1.3	1.3
OPEN F	OPEN F	OPEN F	OPEN F	OPEN F	OPEN F	OPEN F
OPEN	OPEN	OPEN	OPEN	OPEN	OPEN	OPEN
MURID	MURID	MURID	MURID	MURID	MURID	MURID
80.3F	79.9F	80.4F	80.3F	80.3F	81.5F	80.7F
81.0	80.3	80.2	80.3	80.4	80.5	80.6
80.3	80.3	80.3	80.3	80.4	80.4	80.4

SYSTEM SPAD

SYSTEM SPAD

SYSTEM SPAD

1

1

TRC ENVIRONMENTAL CONSULTANTS										ALGONQUIN GAS TRANSMISSION COMPANY HANOVER NJ EMISSION COMPLIANCE PROGRAM									
123	01	02	03	04	05	06	07	08	09	10	11	12	13	14	15	16			
1114	CO	OXYGEN	PERCENT		NOX	PPM	CH ₄	PERCENT	PPM	THC	TEMP		STACK	TEMP					
100	PPM	PERCENT			PPM														
06:37:18	7.4	0.4			0.2	0.1			-4.0	16.000	0.0		PPEN F		80.3F				
200		8.2			0.2	0.1			-3.6		-0.1		PPEN		78.7				
300	4.8	7.5			18.9	1.7			-3.9		1.3		MURLD		80.4				
06:37:38	8.0	0.3			0.2	0.1			-4.0	16.000	0.0		PPEN F		80.4F				
200	5.3	7.2			0.2	0.1			-3.7		0.0		PPEN		78.9				
300	4.8	7.5			18.9	1.7			-3.9		1.3		MURLD		80.4				
06:39:55	-0.3	20.3			0.2	0.2			-4.0	16.000	1.3		PPEN F		79.9F				
200	4.9	6.7			0.2	0.1			-3.7		0.4		PPEN		79.4				
300	5.0	7.5			16.2	1.7			-3.9		1.3		MURLD		80.4				
06:41:54	-0.4	21.4			0.0	0.2			-2.0	4.0000	0.7		PPEN F		79.9F				
200	-0.5	21.2			0.1	-0.2			-3.6		1.0		PPEN		79.2				
300	5.0	8.2			13.8	1.7			-3.9		1.3		MURLD		80.4				
06:44:05	-0.3	21.4			0.2	0.1			-4.0	16.000	11.9		PPEN F		79.4F				
200	-0.4	20.9			0.1	0.1			-3.8		5.0		PPEN		79.3				
300	5.0	9.2			11.1	1.7			-3.9		1.5		MURLD		80.4				
06:45:50	-0.2	21.5			0.0	0.1			-4.0	16.000	0.0		PPEN F		79.3F				
200	-0.2	21.5			0.1	0.1			-4.0		0.0		PPEN		79.3				
300	5.0	9.2			11.1	1.7			-3.9		1.5		MURLD		80.4				
06:47:15	-0.3	7.6			0.0	0.1			-2.0	4.0000	0.0		PPEN F		79.2F				
200	-0.2	16.7			0.0	0.1			-4.0		4.4		PPEN		79.0				
300	5.0	9.6			11.1	1.7			-3.9		1.1		MURLD		80.4				

IN THE STACK

IN THE STACK

07:06:00	8.2	17.5			64.7	2.2		-4.0	16.000	0.0			PPEN F		78.5F	
200	8.2	17.5			64.5	2.2		-4.0		0.0			PPEN		78.0	
300	3.8	14.1			17.2	0.8		-3.9		0.7			MURLD		79.4	
07:08:00	7.6	17.5			64.7	2.3		-4.0	16.000	-0.1			PPEN F		77.9F	
200	7.8	17.5			64.6	2.3		-3.5		-0.1			PPEN		78.3	
300	3.7	14.7			19.4	0.8		-3.9		0.8			MURLD		79.3	
07:10:00	7.2	17.4			65.5	2.3		-4.0	16.000	-0.2			PPEN F		78.5F	
200	7.6	17.4			65.3	2.3		-3.5		-0.1			PPEN		78.4	
300	4.0	14.5			21.6	0.9		-3.9		0.8			MURLD		79.3	

TRC ENVIRONMENTAL CONSULTANTS				ALGONQUIN GAS TRANSMISSION COMPANY HANDOVER NJ EMISSION COMPLIANCE PROGRAM											
123	01	02	03	04	05	06	07	08	09	10	11	12	13	14	15
1114	CO	OXYGEN	NOX	CO2	CO	PPH	PERCENT	PPH	PPH	TAC	PPH	STACK	WELLS		
100	PPM	PERCENT	PPM	PERCENT	PPM							TEMP	TEMP		
200															
07:12:00	6.9	17.4	66.7	2.3	-4.0	16.000	-0.1					OPEN F	78.5F		
200	6.8	17.4	66.3	2.3	-4.0		-0.1					OPEN	78.3		
300	4.2	14.4	23.8	1.0	-3.9		0.4					WORLD	79.3		
07:14:00	7.1	17.4	65.7	2.3	-4.0	16.000	0.0					OPEN F	78.3F		
200	6.6	17.4	66.3	2.3	-4.0		0.0					OPEN	78.5		
300	4.4	14.3	26.0	1.1	-3.9		0.4					WORLD	79.3		
07:16:00	6.3	17.5	67.0	2.2	-4.0	16.000	0.0					OPEN F	78.7F		
200	6.6	17.4	66.3	2.2	-3.9		0.0					OPEN	78.1		
300	4.3	14.1	28.2	1.1	-3.9		0.4					WORLD	79.2		
07:18:00	5.5	17.7	63.2	1.9	-4.0	16.000	0.0					OPEN F	79.1F		
200	6.1	17.5	64.0	2.1	-3.8		0.0					OPEN	79.2		
300	4.5	14.7	30.3	1.2	-3.9		0.4					WORLD	79.1		
07:20:00	4.8	18.3	52.0	1.8	-4.0	16.000	0.1					OPEN F	78.6F		
200	5.4	17.8	59.7	1.9	-3.7		0.0					OPEN	78.9		
300	4.6	15.3	32.0	1.2	-3.9		0.4					WORLD	79.0		
07:22:00	4.8	18.3	50.7	1.8	-4.0	16.000	0.1					OPEN F	78.7F		
200	4.8	18.3	50.3	1.8	-4.0		0.0					OPEN	78.7		
300	4.8	15.9	31.3	1.3	-3.9		0.5					WORLD	79.0		
07:24:00	4.7	18.3	52.0	1.8	-4.0	16.000	0.1					OPEN F	78.2F		
200	4.7	18.3	50.8	1.8	-4.0		0.0					OPEN	78.3		
300	5.0	16.5	28.6	1.4	-3.9		0.5					WORLD	78.9		
07:26:00	5.1	18.0	49.5	1.9	-2.0	4.0000	0.0					OPEN F	78.0F		
200	4.6	18.3	50.2	1.8	-3.8		0.0					OPEN	78.5		
300	5.2	16.6	26.2	1.4	-3.9		0.5					WORLD	78.8		
07:28:00	4.3	18.4	52.0	1.8	-4.0	16.000	0.0					OPEN F	78.6F		
200	4.6	18.2	53.9	1.8	-4.0		0.0					OPEN	77.9		
300	5.3	16.4	27.9	1.5	-3.9		0.5					WORLD	78.8		
07:30:00	4.7	18.4	49.5	1.8	-4.0	16.000	0.0					OPEN F	78.5F		
200	4.5	18.3	51.9	1.8	-3.9		0.0					OPEN	77.9		
300	5.5	17.0	29.5	1.1	-3.9		0.5					WORLD	78.7		

SPRT 1-12
0720

TEST 2-1 0730 11/14/00

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TRC ENVIRONMENTAL CONSULTANTS ALGONQUIN GAS TRANSMISSION COMPANY HANOVER NJ EMISSION COMPLIANCE PROGRAM

123 1114 100 200 07:48:00 200 300 07:50:00 200 300 07:52:00 200 300 07:54:00 200 300 07:56:00 200 300 07:58:00 200 300 08:00:00 200 300 08:02:00 200 300 08:04:00 200 300 08:06:00 200 300

01	02	03	04	05	06	07	08	09	10	11	12	13	14	15	16
CO	CD	PPM	PPM	PPM	PPM	PERCENT	PERCENT	PPM	PPM	PPM	PPM	PPM	PPM	PPM	PPM
5.7	5.8	4.9	18.0	59.0	2.0	2.0	2.0	-4.0	16.000	0.1	0.1	0.1	0.1	0.1	0.1
5.8	5.8	4.9	17.8	62.9	2.0	2.0	2.0	-23.1	16.000	0.8	0.8	0.8	0.8	0.8	0.8
4.9	4.9	4.9	18.5	47.1	1.7	1.7	1.7	-3.7	16.000	0.1	0.1	0.1	0.1	0.1	0.1
4.9	4.9	4.9	18.1	58.0	1.9	1.9	1.9	-4.0	16.000	0.2	0.2	0.2	0.2	0.2	0.2
5.2	5.2	5.2	18.0	59.8	1.9	1.9	1.9	-3.6	16.000	0.2	0.2	0.2	0.2	0.2	0.2
5.1	5.1	5.1	18.4	49.0	1.7	1.7	1.7	-3.7	16.000	0.1	0.1	0.1	0.1	0.1	0.1
5.5	5.5	5.5	18.2	52.5	2.0	2.0	2.0	-4.0	16.000	1.2	1.2	1.2	1.2	1.2	1.2
5.0	5.0	5.0	18.1	56.3	1.8	1.8	1.8	-3.5	16.000	0.5	0.5	0.5	0.5	0.5	0.5
5.3	5.3	5.3	18.3	50.8	1.8	1.8	1.8	-3.7	16.000	0.1	0.1	0.1	0.1	0.1	0.1
7.0	7.0	7.0	17.3	70.0	2.4	2.4	2.4	-2.0	4.0000	0.3	0.3	0.3	0.3	0.3	0.3
5.7	5.7	5.7	17.9	58.1	2.0	2.0	2.0	-3.3	4.0000	0.1	0.1	0.1	0.1	0.1	0.1
5.5	5.5	5.5	18.2	53.1	1.9	1.9	1.9	-3.7	4.0000	0.1	0.1	0.1	0.1	0.1	0.1
7.2	7.2	7.2	17.3	73.5	2.4	2.4	2.4	-2.0	16.000	0.3	0.3	0.3	0.3	0.3	0.3
7.1	7.1	7.1	17.3	72.3	2.4	2.4	2.4	-3.1	16.000	0.2	0.2	0.2	0.2	0.2	0.2
5.8	5.8	5.8	18.0	55.5	1.9	1.9	1.9	-3.7	16.000	0.1	0.1	0.1	0.1	0.1	0.1
7.2	7.2	7.2	17.2	72.5	2.4	2.4	2.4	-4.0	16.000	0.2	0.2	0.2	0.2	0.2	0.2
7.1	7.1	7.1	17.2	72.4	2.4	2.4	2.4	-3.4	16.000	0.2	0.2	0.2	0.2	0.2	0.2
5.9	5.9	5.9	17.9	58.0	2.0	2.0	2.0	-3.7	16.000	0.1	0.1	0.1	0.1	0.1	0.1
7.0	7.0	7.0	17.3	72.5	2.4	2.4	2.4	-2.0	4.0000	-0.3	-0.3	-0.3	-0.3	-0.3	-0.3
6.7	6.7	6.7	17.3	72.3	2.4	2.4	2.4	-3.3	4.0000	0.1	0.1	0.1	0.1	0.1	0.1
5.8	5.8	5.8	17.9	58.4	2.0	2.0	2.0	-3.6	4.0000	0.1	0.1	0.1	0.1	0.1	0.1
7.1	7.1	7.1	17.3	71.5	2.4	2.4	2.4	-4.0	4.0000	0.1	0.1	0.1	0.1	0.1	0.1
6.9	6.9	6.9	17.3	71.8	2.4	2.4	2.4	-2.8	4.0000	0.1	0.1	0.1	0.1	0.1	0.1
5.7	5.7	5.7	17.9	58.7	2.0	2.0	2.0	-3.6	4.0000	0.1	0.1	0.1	0.1	0.1	0.1
6.6	6.6	6.6	17.5	68.2	2.2	2.2	2.2	-4.0	16.000	0.1	0.1	0.1	0.1	0.1	0.1
6.8	6.8	6.8	17.3	71.2	2.3	2.3	2.3	-2.8	16.000	0.1	0.1	0.1	0.1	0.1	0.1
5.7	5.7	5.7	17.9	58.9	2.0	2.0	2.0	-3.6	16.000	0.1	0.1	0.1	0.1	0.1	0.1
6.4	6.4	6.4	17.5	68.8	2.2	2.2	2.2	-4.0	16.000	1.0	1.0	1.0	1.0	1.0	1.0
6.5	6.5	6.5	17.5	68.0	2.2	2.2	2.2	-3.0	16.000	0.3	0.3	0.3	0.3	0.3	0.3
5.6	5.6	5.6	17.9	59.0	2.0	2.0	2.0	-3.6	16.000	0.1	0.1	0.1	0.1	0.1	0.1

CEM Port 2

1

TRC ENVIRONMENTAL CONSULTANTS ALGONQUIN GAS TRANSMISSION COMPANY HANOVER NJ EMISSION COMPLIANCE PROGRAM

123 1114 100 200	01 02 PPH	03 04 PPH	05 06 PPH	07 08 PPH	09 10 PPH	11 12 PPH	13 14 PPH	15 16 PPH
08:08:00	6.9	17.5	68.2	2.3	-2.0	16.000	0.2	77.8F
200	6.7	17.5	68.3	2.2	-3.1		0.4	77.3
300	5.6	17.9	59.1	2.0	-3.6		0.1	77.8
08:10:00	6.6	17.5	69.5	2.2	-4.0	16.000	0.9	76.7F
200	6.5	17.5	69.1	2.2	-3.3		0.3	76.8
300	5.6	17.9	59.2	2.0	-3.6		0.2	77.7
08:12:00	7.8	18.0	63.8	2.0	-2.0	4.0000	0.5	77.9F
200	6.5	17.6	67.3	2.1	-3.2		0.5	77.3
300	5.7	17.9	59.1	2.0	-3.5		0.2	77.7
08:14:00	6.8	17.5	68.0	2.3	-2.0	4.0000	1.1	78.1F
200	6.5	17.6	67.0	2.1	-3.2		0.5	77.5
300	5.7	17.9	59.1	2.0	-3.4		0.2	77.7
08:16:00	6.7	17.5	68.8	2.2	-2.0	4.0000	0.7	78.2F
200	6.9	17.5	67.8	2.2	-3.3		0.5	78.0
300	5.7	17.9	59.3	2.0	-3.4		0.2	77.7
08:18:00	6.9	17.5	69.0	2.2	-4.0	16.000	4.3	78.1F
200	6.8	17.5	68.5	2.2	-3.4		1.1	78.1
300	5.8	17.8	59.9	2.0	-3.4		0.1	77.7
08:20:00	6.9	17.5	68.8	2.3	-4.0	16.000	1.3	78.3F
200	6.5	17.5	68.4	2.2	-3.3		1.2	78.4
300	5.8	17.8	60.5	2.0	-3.4		0.1	77.6
08:22:00	7.8	17.4	72.2	2.3	-4.0	16.000	4.2	78.1F
200	6.8	17.4	69.7	2.2	-3.2		2.4	78.0
300	6.0	17.8	61.2	2.0	-3.4		0.3	77.6
08:24:00	7.9	17.3	88.8	2.3	-4.0	16.000	0.3	78.7F
200	7.1	17.4	74.3	2.2	-3.4		2.4	78.2
300	6.0	17.8	62.5	2.1	-3.4		0.3	77.7
08:26:00	14.3	17.5	82.5	2.2	-4.0	16.000	6.9	78.7F
200	12.2	17.4	88.5	2.1	-3.8		4.9	78.9
300	6.4	17.7	63.5	2.1	-3.4		0.5	77.7

FLAME
OUT

CEM PORTS

123	TRC	EMISSIONS	CONSULTANTS	04	05	06	07	08	09	10	11	12	13
TIME	PPM	PERCENT	PPM	PPM	PPM	PPM	PPM	PPM	PPM	PPM	PPM	PPM	PPM
08:28:00	18.8	17.3	74.0	2.3	-4.0	16.000	19.9	PPEN F					
200	17.8	17.4	82.5	2.2	-3.8	10.4	PPEN						
300	6.8	17.7	64.3	2.1	-3.4	1.2	PPEN						
08:30:00	31.0	17.2	75.2	2.3	-4.0	16.000	31.4	PPEN F					
200	26.6	17.2	75.0	2.3	-3.6	28.0	PPEN						
300	7.7	17.7	65.2	2.1	-3.4	2.2	PPEN						
08:32:00	55.7	17.1	74.7	2.3	-4.0	16.000	54.6	PPEN F					
200	37.9	17.1	74.8	2.3	-3.6	38.3	PPEN						
300	9.4	17.6	66.0	2.1	-3.4	4.0	PPEN						
08:34:00	67.3	17.1	75.7	2.4	-4.0	16.000	59.8	PPEN F					
200	50.9	17.1	75.0	2.3	-3.7	45.6	PPEN						
300	11.5	17.6	66.8	2.1	-3.5	6.0	PPEN						
08:36:00	99.9	17.0	76.7	2.5	-4.0	16.000	79.1	PPEN F					
200	83.0	17.0	75.8	2.4	-3.6	67.9	PPEN						
300	14.7	17.5	67.7	2.2	-3.5	8.7	PPEN						
08:37:36	42.6	17.0	77.2	2.5	-4.0	16.000	17.2	PPEN F					
200	67.3	17.0	76.2	2.4	-3.9	61.6	PPEN						
300	14.7	17.5	67.7	2.2	-3.5	8.7	PPEN						
08:38:00	80.0	16.9	78.2	2.5	-4.0	16.000	7.6	PPEN F					
200	65.8	16.9	76.4	2.4	-3.9	54.9	PPEN						
300	17.2	17.5	68.7	2.2	-3.5	8.9	PPEN						
08:40:00	42.7	17.0	76.0	2.5	-4.0	16.000	108.9	PPEN F					
200	38.8	17.0	75.9	2.4	-3.3	81.1	PPEN						
300	18.5	17.4	69.7	2.2	-3.6	12.5	PPEN						
08:42:00	53.5	17.8	76.0	2.5	-3.0	4.0000	35.6	PPEN F					
200	49.5	17.4	70.6	2.2	-3.6	12.8	PPEN						
300	20.1	17.4	70.6	2.2	-3.6	12.8	PPEN						
08:44:00	32.5	17.1	76.7	2.4	-4.0	16.000	35.7	PPEN F					
200	49.5	17.0	76.0	2.4	-3.0	16.000	13.9	PPEN					
300	20.9	17.4	71.1	2.2	-3.6	13.9	PPEN						

TRC ENVIRONMENTAL CONSULTANTS, AIR QUALITY GAS TRANSMISSION COMPANY HANOVER NJ EMISSIONS COMPLIANCE PROGRAM

123	01	02	03	04	05	06	07	08	09	10	11	12	13	14	15	16
1114	01	02	03	04	05	06	07	08	09	10	11	12	13	14	15	16
100	01	02	03	04	05	06	07	08	09	10	11	12	13	14	15	16
200	01	02	03	04	05	06	07	08	09	10	11	12	13	14	15	16
	PPM	PPM	PERCENT	PERCENT	PPM	PPM	PERCENT	PERCENT	PPM	PPM	PPM	PPM	PPM	PPM	PPM	PPM
08:46:00	48.9		17.1		75.5		2.4		-4.0	16.000	24.0		PPM F		78.1F	
200	53.9		17.1		75.8		2.4		-3.1		29.1		PPM		77.8	
300	22.4		17.3		71.5		2.2		-3.6		14.7		MURI D		77.6	
08:48:00	36.6		17.3		75.2		2.3		-4.0	16.000	22.4		PPM F		77.2F	
200	46.3		17.1		75.6		2.3		-3.0		26.9		PPM		77.8	
300	23.4		17.3		72.0		2.3		-3.6		15.5		MURI D		77.6	
08:50:00	24.6		17.3		72.0		2.3		-4.0	16.000	15.2		PPM F		77.1F	
200	27.4		17.3		72.4		2.3		-2.6		16.9		PPM		77.2	
300	24.0		17.3		72.5		2.3		-3.6		16.0		MURI D		77.6	
08:52:00	29.0		19.9		60.2		0.5		-2.0	4.0000	11.9		PPM F		76.6F	
200	23.7		17.6		72.3		1.9		-2.4		14.9		PPM		76.9	
300	24.8		17.4		72.7		2.2		-3.5		16.3		MURI D		77.6	
08:54:00	4.4		21.2		1.5		0.2		-2.0	4.0000	9.4		PPM F		77.2F	
200	18.1		18.9		49.8		1.2		-2.3		13.0		PPM		77.0	
300	24.7		17.5		70.4		2.1		-3.4		16.6		MURI D		77.6	
08:56:00	6.3		21.3		0.2		0.2		-2.0	4.0000	12.5		PPM F		77.4F	
200	4.4		21.2		0.5		0.2		-3.0		10.3		PPM		77.4	
300	24.7		17.6		68.0		2.1		-3.4		17.0		MURI D		77.6	
08:58:00	14.5		21.3		0.2		0.2		-4.0	16.000	17.5		PPM F		78.3F	
200	7.2		21.2		0.3		0.2		-3.1		13.3		PPM		77.5	
300	25.0		17.7		65.6		2.0		-3.4		17.6		MURI D		77.6	
09:03:18	-0.2		22.3		0.0		0.1		-3.0	4.0000	2.5		PPM F		77.7F	
200	24.9		18.5		60.8		1.8		-3.4		18.1		MURI D		77.7	
300			17.3													
09:07:42	-0.6		22.3		0.0		0.1		-2.0	4.0000	0.2		PPM F		78.2F	
200	-0.6		18.5		0.0		0.1		-2.9		0.2		PPM		78.0	
300	24.4		16.6		56.2		1.7		-3.2		18.1		MURI D		77.7	
09:11:36	-1.3		0.0		0.2		0.2		-2.0	4.0000	0.9		PPM F		77.7F	
200	-1.0		10.7		0.1		0.2		-2.8		0.9		PPM		77.8	
300	23.9		16.8		51.6		1.8		-3.2		18.1		MURI D		77.8	

TEST 2-1 COMPLETED

SYSTEM ZERO

SYSTEM SPAD

SYSTEM SPAD

ALUMINUM GAS TRANSMISSION COMPANY HANOVER NJ EMISSION COMPLIANCE PROGRAM

123 TRC ENVIRONMENTAL CONSULTANTS
1114 N1 N2 N3 N4
1000 N5 N6 N7 N8 N9 N10 N11 N12 N13 N14 N15
2000 N17 N18 N19 N20 N21 N22 N23 N24 N25 N26 N27 N28 N29 N30

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IN THE STACK

TEST 2-2 START 1650-38M

TEST 2-2 START 0955 CEM PORT 4

SYSTEM
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SYSTEM
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SYSTEM
SPAD

TRC ENVIRONMENTAL CONSULTANTS AIR EMISSION GAS TRANSMISSION COMPANY HANDED BY EMISSION COMPLIANCE PROGRAM

123	124	125	126	127	128	129	130	131	132	133	134	135	136
TIME	CONCENTRATION	PERCENT	PERCENT	PPM	PPM	PERCENT	PPM	PPM	PPM	PPM	PPM	PPM	PPM
10:01:00	6.8	17.2	17.2	73.5	73.5	2.5	-2.0	4.0000	0.1	PPEN F	78.9F	78.9	78.9
200	7.0	17.1	17.1	73.2	73.2	2.5	-2.4		0.3	PPEN	78.8	78.8	78.8
300	2.7	14.2	14.2	31.1	31.1	1.5	-2.8		1.0	MURID	78.2	78.2	78.2
10:03:00	6.9	17.2	17.2	73.2	73.2	2.5	-2.0	4.0000	0.1	PPEN F	79.1F	79.1	79.1
200	7.0	17.1	17.1	73.2	73.2	2.5	-2.4		0.2	PPEN	78.8	78.8	78.8
300	3.0	14.7	14.7	33.6	33.6	1.5	-2.8		0.9	MURID	78.2	78.2	78.2
10:05:00	7.1	17.2	17.2	72.7	72.7	2.5	-2.0	4.0000	0.3	PPEN F	79.9F	79.9	79.9
200	6.9	17.2	17.2	72.6	72.6	2.5	-2.8		0.2	PPEN	79.6	79.6	79.6
300	3.2	14.9	14.9	36.0	36.0	1.6	-2.8		0.9	MURID	78.3	78.3	78.3
10:07:00	6.1	17.2	17.2	74.5	74.5	2.5	-2.0	4.0000	0.4	PPEN F	78.7F	78.7	78.7
200	6.9	17.2	17.2	73.0	73.0	2.5	-2.4		0.3	PPEN	78.6	78.6	78.6
300	3.5	14.7	14.7	38.5	38.5	1.7	-2.8		1.0	MURID	78.3	78.3	78.3
10:09:00	2.3	13.2	13.2	74.2	74.2	2.5	-2.0	4.0000	0.2	PPEN F	78.7F	78.7	78.7
200	3.7	14.7	14.7	41.0	41.0	1.5	-2.8		0.9	MURID	78.4	78.4	78.4
10:11:00	6.7	17.2	17.2	75.0	75.0	2.5	-2.0	4.0000	0.5	PPEN F	78.6F	78.6	78.6
200	6.7	17.1	17.1	74.0	74.0	2.5	-2.3		0.2	PPEN	78.7	78.7	78.7
300	4.0	15.2	15.2	43.5	43.5	1.2	-2.8		0.9	MURID	78.4	78.4	78.4
10:13:00	6.8	17.1	17.1	74.7	74.7	2.5	-4.0	16.0000	0.2	PPEN F	79.2F	79.2	79.2
200	6.8	17.1	17.1	74.2	74.2	2.5	-2.7		0.2	PPEN	78.8	78.8	78.8
300	4.3	15.8	15.8	43.5	43.5	1.2	-2.8		0.9	MURID	78.4	78.4	78.4
10:15:00	6.5	17.1	17.1	74.0	74.0	2.5	-4.0	16.0000	0.6	PPEN F	80.3F	80.3	80.3
200	6.5	17.1	17.1	74.1	74.1	2.5	-3.6		0.1	PPEN	80.0	80.0	80.0
300	4.5	16.4	16.4	41.6	41.6	1.3	-2.8		0.9	MURID	78.5	78.5	78.5
10:17:00	10.7	18.3	18.3	31.3	31.3	2.3	-2.0	4.0000	0.9	PPEN F	80.0F	80.0	80.0
200	7.7	17.7	17.7	66.8	66.8	2.1	-3.7		1.4	PPEN	80.0	80.0	80.0
300	4.9	17.0	17.0	38.2	38.2	1.4	-2.8		0.9	MURID	78.5	78.5	78.5
10:19:00	7.6	17.1	17.1	76.5	76.5	2.5	-4.0	16.0000	0.3	PPEN F	79.6F	79.6	79.6
200	7.7	17.1	17.1	76.4	76.4	2.5	-3.6		0.4	PPEN	79.7	79.7	79.7
300	4.9	17.6	17.6	38.6	38.6	1.4	-2.8		0.9	MURID	78.6	78.6	78.6

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TRC ENVIRONMENTAL CONSULTANTS ALGONQUIN GAS TRANSMISSION COMPANY HANOVER NJ EMISSION COMPLIANCE PROGRAM

123 1114	01 02	03 04	05 06	07 08	09 10	11 12	13 14	15 16
TIME	CON PPM	NOX PPM	CO PPM	PERCENT	PPM	PPM	STACK TEMP	WFLS TEMP
10:21:00	6.4	17.1	76.5	2.5	-2.0	4.0000	NPEN F	79.6F
200	7.0	17.1	76.9	2.5	-3.1		NPEN	79.6
300	4.9	18.1	41.2	1.5	-2.7		MURLD	78.6
10:23:00	6.4	17.1	75.2	2.5	-4.0	16.0000	NPEN F	80.3F
200	6.8	17.1	76.3	2.5	-3.0		NPEN	79.7
300	4.9	18.7	43.7	1.6	-2.6		MURLD	78.7
10:25:00	6.6	17.1	74.0	2.5	-4.0	16.0000	NPEN F	79.3F
200	6.5	17.1	74.7	2.5	-3.0		NPEN	79.8
300	5.1	18.6	46.1	1.7	-2.6		MURLD	78.8
10:27:00	6.5	17.1	74.7	2.5	-2.0	4.0000	NPEN F	79.8F
200	6.5	17.1	74.6	2.5	-2.7		NPEN	79.8
300	5.4	18.4	48.6	1.8	-2.6		MURLD	78.9
10:29:00	6.3	17.1	73.8	2.5	-4.0	4.0000	NPEN F	78.7F
200	6.3	17.1	74.5	2.5	-2.0		NPEN	78.5
300	5.6	18.3	51.1	1.8	-2.6		MURLD	78.9
10:31:00	7.0	17.1	72.2	2.5	-2.0	4.0000	NPEN F	79.9F
200	6.4	17.1	73.1	2.5	-2.4		NPEN	79.1
300	5.8	18.1	53.5	1.9	-2.6		MURLD	78.9
10:33:00	6.6	17.1	72.7	2.5	-2.0	16.0000	NPEN F	78.6F
200	6.4	17.1	72.7	2.5	-2.6		NPEN	78.8
300	6.1	18.0	55.9	2.0	-2.6		MURLD	78.9
10:35:00	6.5	17.1	71.7	2.5	-4.0	4.0000	NPEN F	77.3F
200	6.3	17.1	72.4	2.5	-2.6		NPEN	78.3
300	6.3	17.8	58.3	2.1	-2.6		MURLD	78.9
10:37:00	6.4	17.1	73.8	2.5	-2.0	4.0000	NPEN F	77.6F
200	6.4	17.1	72.3	2.5	-2.6		NPEN	77.6
300	6.6	17.7	60.8	2.1	-2.6		MURLD	78.9
10:39:00	9.9	19.5	54.2	1.8	-4.0	16.0000	NPEN F	77.2F
200	7.7	18.2	69.4	1.5	-2.6		NPEN	78.0
300	6.9	17.6	62.7	2.2	-2.6		MURLD	78.9

OUT OF STACK
AS IN ART 2

TRC ENVIRONMENTAL CONSULTANTS ALGHOJIN GAS TRANSMISSION COMPANY HANOVER NJ EMISSION COMPLIANCE PROGRAM

123	124	125	126	127	128	129	130	131	132	133	134	135	136
TAC ENVIRONMENTAL CONSULTANTS	ALCONQUIN GAS TRANSMISSION COMPANY HANOVER NJ EMISSION COMPLIANCE PROGRAM												
N1 PPM	N2 PPM	N3 PERCENT	N4 PERCENT	N5 PPM	N6 PPM	N7 PERCENT	N8 PPM	N9 PPM	N10 PPM	N11 THC	N12 TEMP	N13 STAGE	N14 TEMP
10:41:00	6.7	17.2	17.2	76.7	-2.0	2.5	4.0000	0.1	NPEN F				79.0F
200	8.4	17.8	17.8	64.3	-2.8	2.1		0.8	NPEN				78.3
300	7.2	17.5	17.5	65.2	-2.6	2.3		0.3	MURID				78.9
10:43:00	6.6	17.1	17.1	74.2	-2.0	2.5	4.0000	-0.2	NPEN F				78.0F
200	7.7	17.5	17.5	68.3	-2.9	2.2		0.4	NPEN				78.4
300	7.4	17.4	17.4	67.7	-2.6	2.4		0.2	MURID				78.9
10:45:00	6.9	17.1	17.1	72.0	-2.0	2.5	4.0000	-0.2	NPEN F				79.2F
200	6.6	17.1	17.1	72.6	-2.6	2.5		-0.1	NPEN				79.1
300	7.3	17.3	17.3	69.1	-2.6	2.4		0.2	MURID				78.9
10:47:00	6.8	17.1	17.1	72.2	-4.0	2.5	16.0000	-0.2	NPEN F				78.6F
200	6.6	17.1	17.1	72.4	-2.8	2.5		-0.1	NPEN				79.0
300	7.2	17.3	17.3	69.9	-2.6	2.4		0.1	MURID				78.9
10:49:00	7.8	17.1	17.1	71.0	-2.0	2.5	4.0000	-0.2	NPEN F				76.2F
200	6.8	17.1	17.1	71.4	-3.3	2.5		-0.2	NPEN				77.9
300	7.1	17.2	17.2	70.7	-2.5	2.4		0.1	MURID				78.8
10:51:00	6.5	17.1	17.1	72.2	-4.0	2.5	16.0000	-0.4	NPEN F				76.6F
200	6.6	17.1	17.1	71.5	-3.2	2.5		-0.3	NPEN				76.4
300	7.0	17.2	17.2	71.6	-2.6	2.4		0.1	MURID				78.7
10:53:00	6.3	17.1	17.1	72.5	-4.0	2.5	16.0000	-0.6	NPEN F				79.5F
200	6.5	17.1	17.1	72.1	-3.2	2.5		-0.3	NPEN				77.2
300	7.0	17.2	17.2	71.7	-2.6	2.4		0.1	MURID				78.8
10:55:00	6.3	17.1	17.1	71.5	-2.0	2.5	4.0000	-0.4	NPEN F				79.0F
200	6.2	17.1	17.1	72.1	-3.1	2.5		-0.3	NPEN				79.2
300	7.0	17.2	17.2	71.6	-2.6	2.4		0.0	MURID				78.8
10:57:00	6.5	17.1	17.1	71.5	-4.0	2.5	16.0000	-0.4	NPEN F				77.9F
200	6.3	17.1	17.1	71.8	-3.3	2.5		-0.3	NPEN				78.9
300	6.9	17.2	17.2	71.5	-2.6	2.4		0.0	MURID				78.8
10:59:00	6.0	17.1	17.1	71.5	-4.0	2.5	16.0000	-0.4	NPEN F				78.2F
200	6.3	17.1	17.1	71.5	-2.6	2.5		-0.3	NPEN				78.3
300	6.9	17.2	17.2	71.5	-2.7	2.4		0.0	MURID				78.8

123	TRC ENVIRONMENTAL CONSULTANTS			ALIGNMENT GAS TRANSMISSION COMPANY HANOVER NJ EMISSION COMPLIANCE PROGRAM											
	01	02	03	04	05	06	07	08	09	10	11	12	13	14	15
100	01	02	03	04	05	06	07	08	09	10	11	12	13	14	15
200	PPM	PERCENT	PERCENT	PPM	PPM	PERCENT	PERCENT	PPM	PPM	PPM	PPM	PPM	STACK	TEMP	WET
11:01:00	6.5	17.1	17.1	67.0	67.0	2.5	2.5	-2.0	4.0000	-0.2	-0.2	PPEN F	PPEN F	78.4F	
200	6.3	17.1	17.1	70.8	70.8	2.5	2.5	-3.2		-0.3	-0.3	PPEN	PPEN	78.5	
300	6.9	17.2	17.2	71.3	71.3	2.4	2.4	-2.7		0.0	0.0	MURID	MURID	78.7	
11:03:00	6.5	17.1	17.1	66.5	66.5	2.5	2.5	-4.0	16.000	-0.4	-0.4	PPEN F	PPEN F	78.5F	
200	6.5	17.1	17.1	69.2	69.2	2.5	2.5	-3.2		-0.3	-0.3	PPEN	PPEN	78.4	
300	6.8	17.2	17.2	71.0	71.0	2.4	2.4	-2.8		0.0	0.0	MURID	MURID	78.7	
11:05:00	7.1	17.4	17.4	60.7	60.7	2.5	2.5	-2.0	4.0000	0.1	0.1	PPEN F	PPEN F	78.4F	
200	6.8	17.2	17.2	65.8	65.8	2.3	2.3	-3.1		-0.1	-0.1	PPEN	PPEN	78.3	
300	6.8	17.2	17.2	70.6	70.6	2.4	2.4	-2.8		0.0	0.0	MURID	MURID	78.7	
11:07:00	6.2	17.1	17.1	71.7	71.7	2.5	2.5	-2.0	4.0000	-0.5	-0.5	PPEN F	PPEN F	79.2F	
200	6.6	17.2	17.2	67.4	67.4	2.4	2.4	-3.2		-0.3	-0.3	PPEN	PPEN	78.5	
300	6.9	17.2	17.2	70.5	70.5	2.4	2.4	-2.8		0.0	0.0	MURID	MURID	78.7	
11:09:00	6.8	17.1	17.1	70.5	70.5	2.5	2.5	-4.0	16.000	-0.1	-0.1	PPEN F	PPEN F	78.9F	
200	6.5	17.1	17.1	71.0	71.0	2.5	2.5	-3.3		-0.2	-0.2	PPEN	PPEN	78.9	
300	6.8	17.2	17.2	70.4	70.4	2.4	2.4	-2.8		0.0	0.0	MURID	MURID	78.7	
11:11:00	6.5	17.1	17.1	70.0	70.0	2.5	2.5	-4.0	16.000	-0.3	-0.3	PPEN F	PPEN F	79.2F	
200	6.5	17.1	17.1	70.8	70.8	2.5	2.5	-3.2		-0.2	-0.2	PPEN	PPEN	79.0	
300	6.8	17.2	17.2	70.3	70.3	2.4	2.4	-2.9		0.0	0.0	MURID	MURID	78.7	
11:13:00	6.9	17.1	17.1	71.5	71.5	2.5	2.5	-4.0	16.000	-0.4	-0.4	PPEN F	PPEN F	79.7F	
200	6.6	17.1	17.1	71.0	71.0	2.5	2.5	-3.3		-0.2	-0.2	PPEN	PPEN	79.2	
300	6.8	17.2	17.2	70.1	70.1	2.4	2.4	-2.9		0.0	0.0	MURID	MURID	78.7	
11:15:00	6.4	17.1	17.1	70.2	70.2	2.5	2.5	-4.0	16.000	-0.4	-0.4	PPEN F	PPEN F	79.6F	
200	6.5	17.1	17.1	70.8	70.8	2.5	2.5	-3.1		-0.3	-0.3	PPEN	PPEN	79.7	
300	6.8	17.2	17.2	70.0	70.0	2.4	2.4	-2.9		-0.1	-0.1	MURID	MURID	78.7	
11:17:00	6.2	17.1	17.1	70.5	70.5	2.5	2.5	-4.0	16.000	-0.4	-0.4	PPEN F	PPEN F	80.0F	
200	6.4	17.1	17.1	70.7	70.7	2.5	2.5	-3.4		-0.3	-0.3	PPEN	PPEN	79.8	
300	6.7	17.1	17.1	71.3	71.3	2.4	2.4	-3.0		-0.1	-0.1	MURID	MURID	78.7	
11:19:00	6.6	17.1	17.1	70.7	70.7	2.5	2.5	-4.0	16.000	-0.5	-0.5	PPEN F	PPEN F	79.4F	
200	6.4	17.1	17.1	70.5	70.5	2.5	2.5	-3.6		-0.4	-0.4	PPEN	PPEN	78.7	
300	6.6	17.1	17.1	71.1	71.1	2.4	2.4	-3.0		-0.1	-0.1	MURID	MURID	78.7	

CEM PORT 1

TPO ENVIRONMENTAL CONCENTRANTS				AIRBORNE GAS TRANSMISSION COMPANY				HANDLER NJ EMISSIONS TEMP. JANCE				STACK		WJCS		
123	01	02	03	04	05	06	07	08	09	10	11	12	13	14	15	16
1114	PPM		PERCENT		PPM		PERCENT		PPM		PPM	TEMP	TEMP		TEMP	
100	6.8		17.1		78.8		2.6		-4.0	16.000	-0.4	MPFN F			79.9F	
200	6.6		17.1		78.3		2.5		-3.8		-0.4	MPFN			79.9	
300	1.7		8.0		57.8		1.1		-3.8		1.0	MURLD			79.9	
12:24:00																
200	6.6		17.1		77.0		2.5		-4.0	16.000	-0.3	MPFN F			79.4F	
300	1.9		8.6		60.4		1.2		-3.9		-0.4	MPFN			79.5	
12:26:00									-3.8		1.0	MURLD			79.9	
200	6.4		17.1		76.7		2.5		-4.0	16.000	-0.6	MPFN F			79.8F	
300	2.2		9.2		67.9		1.3		-4.0		-0.4	MPFN			79.8	
12:28:00									-3.8		1.0	MURLD			79.9	
200	6.5		17.1		77.2		2.5		-4.0	16.000	-0.4	MPFN F			79.1F	
300	2.4		9.7		65.5		1.3		-4.0		-0.3	MPFN			79.5	
12:30:00									-3.8		0.9	MURLD			79.9	
200	6.4		17.1		76.8		2.5		-4.0	16.000	-0.4	MPFN F			79.4F	
300	2.4		10.3		64.0		1.4		-4.0		-0.3	MPFN			79.4	
12:32:00									-3.8		0.9	MURLD			79.9	
200	6.5		17.1		75.5		2.5		-4.0	16.000	-0.3	MPFN F			80.6F	
300	2.6		10.3		62.4		1.5		-4.0		-0.4	MPFN			80.1	
12:34:00									-3.8		0.9	MURLD			79.9	
200	6.6		17.2		75.7		2.5		-4.0	16.000	-0.4	MPFN F			80.5F	
300	2.9		10.9		60.7		1.6		-3.9		-0.3	MPFN			80.2	
12:36:00									-3.8		0.8	MURLD			80.0	
200	6.6		17.1		75.8		2.5		-4.0	16.000	-0.3	MPFN F			80.4F	
300	3.1		11.5		60.7		1.7		-4.3		-0.1	MPFN			80.5	
12:38:00									-3.9		0.8	MURLD			80.1	
200	6.8		17.2		75.0		2.5		-4.0	16.000	-0.3	MPFN F			77.2F	
300	3.3		12.0		58.9		1.7		-4.3		-0.2	MPFN			79.8	
12:40:00									-3.8		0.8	MURLD			80.0	
200	6.4		17.2		76.3		2.5		-2.0	4.0000	-0.1	MPFN F			77.2F	
300	3.6		12.6		57.3		1.7		-4.0		-0.2	MPFN			79.8	
12:42:00									-3.8		0.6	MURLD			80.0	
200	6.6		17.2		76.5		2.3		-4.0	16.000	-0.3	MPFN F			80.1F	
300	3.8		13.2		55.6		1.8		-3.8		0.6	MURLD			80.0	

ALGONQUIN GAS TRANSMISSION COMPANY HANOVER NJ EMISSION COMPLIANCE PROGRAM

123	TRC ENVIRONMENTAL CONSULTANTS	04	05	06	07	08	09	10	11	12	13	14	15	16
1114	01	02	03	04	05	06	07	08	09	10	11	12	13	14
100	01	02	03	04	05	06	07	08	09	10	11	12	13	14
200	01	02	03	04	05	06	07	08	09	10	11	12	13	14
300	01	02	03	04	05	06	07	08	09	10	11	12	13	14
12:44:00	01	02	03	04	05	06	07	08	09	10	11	12	13	14
200	01	02	03	04	05	06	07	08	09	10	11	12	13	14
300	01	02	03	04	05	06	07	08	09	10	11	12	13	14
12:46:00	01	02	03	04	05	06	07	08	09	10	11	12	13	14
200	01	02	03	04	05	06	07	08	09	10	11	12	13	14
300	01	02	03	04	05	06	07	08	09	10	11	12	13	14
12:48:00	01	02	03	04	05	06	07	08	09	10	11	12	13	14
200	01	02	03	04	05	06	07	08	09	10	11	12	13	14
300	01	02	03	04	05	06	07	08	09	10	11	12	13	14
12:50:00	01	02	03	04	05	06	07	08	09	10	11	12	13	14
200	01	02	03	04	05	06	07	08	09	10	11	12	13	14
300	01	02	03	04	05	06	07	08	09	10	11	12	13	14
12:52:00	01	02	03	04	05	06	07	08	09	10	11	12	13	14
200	01	02	03	04	05	06	07	08	09	10	11	12	13	14
300	01	02	03	04	05	06	07	08	09	10	11	12	13	14
12:54:00	01	02	03	04	05	06	07	08	09	10	11	12	13	14
200	01	02	03	04	05	06	07	08	09	10	11	12	13	14
300	01	02	03	04	05	06	07	08	09	10	11	12	13	14
12:56:00	01	02	03	04	05	06	07	08	09	10	11	12	13	14
200	01	02	03	04	05	06	07	08	09	10	11	12	13	14
300	01	02	03	04	05	06	07	08	09	10	11	12	13	14
12:58:00	01	02	03	04	05	06	07	08	09	10	11	12	13	14
200	01	02	03	04	05	06	07	08	09	10	11	12	13	14
300	01	02	03	04	05	06	07	08	09	10	11	12	13	14
13:00:00	01	02	03	04	05	06	07	08	09	10	11	12	13	14
200	01	02	03	04	05	06	07	08	09	10	11	12	13	14
300	01	02	03	04	05	06	07	08	09	10	11	12	13	14
13:02:00	01	02	03	04	05	06	07	08	09	10	11	12	13	14
200	01	02	03	04	05	06	07	08	09	10	11	12	13	14
300	01	02	03	04	05	06	07	08	09	10	11	12	13	14

CEM PORT 3

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ALCONQUIN GAS TRANSMISSION COMPANY HANDOVER NJ EMISSION COMPLIANCE PROGRAM

123	124	125	126	127	128	129	130	131	132	133	134	135	136
1114	1115	1116	1117	1118	1119	1120	1121	1122	1123	1124	1125	1126	1127
100	101	102	103	104	105	106	107	108	109	110	111	112	113
200	201	202	203	204	205	206	207	208	209	210	211	212	213
TRC ENVIRONMENTAL CONSULTANTS	ALCONQUIN GAS TRANSMISSION COMPANY	HANDOVER NJ EMISSION COMPLIANCE PROGRAM											
01	02	03	04	05	06	07	08	09	10	11	12	13	14
CO	CO	OXYGEN	NOX	CO2	PPM	PERCENT	PPH	PPH	PPH	THC	TEMP	TEMP	TEMP
PPM	PPM	PERCENT	PPM	PERCENT	PPM	PERCENT	PPH	PPH	PPH	PPM C3	TEMP	TEMP	TEMP
6.6	17.1	66.5	2.5	-4.0	16.000	0.1	OPEN F	83.5F					
6.4	17.1	66.3	2.5	-3.6		0.1	OPEN	82.7					
7.5	17.1	72.5	2.4	-3.4		0.0	DURLD	80.8					
6.6	17.1	66.3	2.5	-4.0	16.000	0.1	OPEN F	83.8F					
6.5	17.1	66.5	2.5	-3.5		0.1	OPEN	83.1					
7.5	17.1	72.1	2.4	-3.4		0.0	DURLD	81.0					
6.7	17.1	67.7	2.5	-4.0	16.000	0.4	OPEN F	82.5F					
6.4	17.1	67.2	2.5	-4.0		0.3	OPEN	81.8					
7.5	17.1	71.8	2.4	-3.4		0.0	DURLD	81.0					
6.8	17.4	64.7	2.5	-4.0	16.000	0.3	OPEN F	83.2F					
6.6	17.1	67.4	2.4	-3.8		0.5	OPEN	82.7					
7.5	17.1	71.4	2.4	-3.4		0.0	DURLD	81.2					
6.2	17.1	68.2	2.5	-4.0	16.000	0.2	OPEN F	83.1F					
6.5	17.1	67.2	2.4	-4.0		0.4	OPEN	82.9					
7.5	17.1	71.1	2.4	-3.4		0.0	DURLD	81.3					
6.3	17.1	67.7	2.5	-4.0	16.000	0.1	OPEN F	83.9F					
7.5	17.1	70.8	2.4	-3.4		0.0	DURLD	81.4					
6.4	17.1	66.5	2.5	-4.0	16.000	0.3	OPEN F	83.7F					
6.3	17.1	67.3	2.5	-3.7		0.2	OPEN	83.3					
7.5	17.1	70.5	2.4	-3.4		0.0	DURLD	81.5					
6.3	17.1	66.5	2.5	-4.0	16.000	0.2	OPEN F	82.7F					
6.3	17.1	66.5	2.5	-4.0		0.2	OPEN	82.3					
7.5	17.1	70.3	2.4	-3.4		0.0	DURLD	81.6					
6.2	17.1	66.7	2.5	-4.0	16.000	0.3	OPEN F	83.2F					
6.3	17.1	66.6	2.5	-4.0		0.2	OPEN	82.8					
7.5	17.1	69.9	2.4	-3.5		0.1	DURLD	81.8					
6.4	17.1	67.2	2.5	-4.0	16.000	0.2	OPEN F	84.0F					
6.2	17.1	66.7	2.5	-4.0		0.2	OPEN	83.3					
7.5	17.1	69.6	2.4	-3.5		0.1	DURLD	81.9					

CEM PORT 1

123	124	125	126	127	128	129	130	131	132	133	134	135	136
1114	1115	1116	1117	1118	1119	1120	1121	1122	1123	1124	1125	1126	1127
100	101	102	103	104	105	106	107	108	109	110	111	112	113
200	201	202	203	204	205	206	207	208	209	210	211	212	213
TRC ENVIRONMENTAL CONSULTANTS	ALGONQUIN GAS TRANSMISSION COMPANY	HANDOVER NJ EMISSION COMPLIANCE PROGRAM											
CO PPM	OXYGEN PERCENT	NOX PPM	CO2 PERCENT	CO PPM	THC PPM	CO PPM	THC PPM	CO PPM	THC PPM	CO PPM	THC PPM	CO PPM	THC PPM
13:44:00	17.1	67.0	2.5	-4.0	0.2	-4.0	0.2	-4.0	0.2	-4.0	0.2	-4.0	0.2
200	17.1	66.8	2.5	-4.0	0.2	-4.0	0.2	-4.0	0.2	-4.0	0.2	-4.0	0.2
300	17.1	69.3	2.4	-3.5	0.1	-3.5	0.1	-3.5	0.1	-3.5	0.1	-3.5	0.1
13:46:00	17.1	67.2	2.5	-4.0	0.5	-4.0	0.5	-4.0	0.5	-4.0	0.5	-4.0	0.5
200	17.1	66.8	2.5	-4.0	0.2	-4.0	0.2	-4.0	0.2	-4.0	0.2	-4.0	0.2
300	17.1	68.9	2.4	-3.5	0.1	-3.5	0.1	-3.5	0.1	-3.5	0.1	-3.5	0.1
13:48:00	17.1	66.5	2.5	-4.0	0.4	-4.0	0.4	-4.0	0.4	-4.0	0.4	-4.0	0.4
200	17.1	66.5	2.5	-4.0	0.2	-4.0	0.2	-4.0	0.2	-4.0	0.2	-4.0	0.2
300	17.1	68.6	2.4	-3.5	0.1	-3.5	0.1	-3.5	0.1	-3.5	0.1	-3.5	0.1
13:50:00	17.1	67.7	2.5	-4.0	0.4	-4.0	0.4	-4.0	0.4	-4.0	0.4	-4.0	0.4
200	17.1	67.2	2.5	-4.0	0.2	-4.0	0.2	-4.0	0.2	-4.0	0.2	-4.0	0.2
300	17.1	68.4	2.4	-3.5	0.1	-3.5	0.1	-3.5	0.1	-3.5	0.1	-3.5	0.1
14:00:11	0.0	1.0	0.1	-6.0	1.4	-6.0	1.4	-6.0	1.4	-6.0	1.4	-6.0	1.4
200	0.0	1.1	0.1	-3.7	1.3	-3.7	1.3	-3.7	1.3	-3.7	1.3	-3.7	1.3
300	14.8	59.0	2.1	-3.6	0.4	-3.6	0.4	-3.6	0.4	-3.6	0.4	-3.6	0.4
14:00:36	0.0	0.7	0.1	-4.0	1.5	-4.0	1.5	-4.0	1.5	-4.0	1.5	-4.0	1.5
200	0.0	1.0	0.1	-3.8	1.3	-3.8	1.3	-3.8	1.3	-3.8	1.3	-3.8	1.3
300	14.8	59.0	2.1	-3.6	0.4	-3.6	0.4	-3.6	0.4	-3.6	0.4	-3.6	0.4
14:01:27	0.0	0.7	0.1	-4.0	1.5	-4.0	1.5	-4.0	1.5	-4.0	1.5	-4.0	1.5
200	0.0	1.0	0.1	-3.7	1.3	-3.7	1.3	-3.7	1.3	-3.7	1.3	-3.7	1.3
300	14.8	59.0	2.1	-3.6	0.4	-3.6	0.4	-3.6	0.4	-3.6	0.4	-3.6	0.4
14:02:00	0.0	1.0	0.1	-4.0	1.5	-4.0	1.5	-4.0	1.5	-4.0	1.5	-4.0	1.5
200	0.0	1.0	0.1	-3.7	1.3	-3.7	1.3	-3.7	1.3	-3.7	1.3	-3.7	1.3
300	14.3	56.5	2.1	-3.6	0.5	-3.6	0.5	-3.6	0.5	-3.6	0.5	-3.6	0.5
14:13:59	0.0	133.0	0.1	-4.0	1.9	-4.0	1.9	-4.0	1.9	-4.0	1.9	-4.0	1.9
200	0.0	176.4	0.1	-3.6	1.7	-3.6	1.7	-3.6	1.7	-3.6	1.7	-3.6	1.7
300	11.4	65.5	1.7	-3.7	0.7	-3.7	0.7	-3.7	0.7	-3.7	0.7	-3.7	0.7
14:17:30	0.0	9.0	0.1	-4.0	0.8	-4.0	0.8	-4.0	0.8	-4.0	0.8	-4.0	0.8
200	0.0	18.9	0.1	-3.7	0.7	-3.7	0.7	-3.7	0.7	-3.7	0.7	-3.7	0.7
300	10.3	69.8	1.5	-3.7	0.7	-3.7	0.7	-3.7	0.7	-3.7	0.7	-3.7	0.7

END TEST 2-3-3

SYSTEM ZERO

SYSTEM ZERO SPAD

SYSTEM SPAN

ALGONQUIN GAS TRANSMISSION COMPANY HANOVER NJ EMISSIONS LABORATORY										13	14	15	16
TREC ENVIRONMENTAL CONSULTANTS										STACK	TEMP	HELS	TEMP
123	01	02	03	04	05	06	07	08	09	10	11	12	13
1114	CO	CO	NOX	PM	PM	PM	PM	PM	PM	PM	PM	PM	PM
100	PPM	PPM	PERCENT	PERCENT	PPM	PPM	PERCENT	PERCENT	PPM	PPM	PPM	PPM	PPM
200	PPM	PPM	PERCENT	PERCENT	PPM	PPM	PERCENT	PERCENT	PPM	PPM	PPM	PPM	PPM
15:01:01	0.1	0.1	0.1	0.1	0.1	0.1	0.2	SYSTEM	-4.0	16.000	0.9	OPEN F	85.9F
200	1.8	4.4	4.4	4.4	4.4	4.4	0.6	ZERO	-4.0	16.000	2.2	OPEN F	85.9F
300	1.8	4.4	4.4	4.4	4.4	4.4	0.6	ZERO	-3.5	16.000	2.2	OPEN F	85.9F
15:07:17	-0.3	0.0	0.0	0.0	0.0	0.0	0.2	SYSTEM	-4.0	16.000	1.0	OPEN F	87.1F
200	-0.1	0.0	0.0	0.0	0.0	0.0	0.2	SYSTEM	-4.0	16.000	1.0	OPEN F	87.1F
300	1.8	4.4	4.4	4.4	4.4	4.4	0.6	SYSTEM	-3.5	16.000	2.1	OPEN F	85.2F
15:10:45	0.0	0.0	0.0	0.0	0.0	0.0	0.2	SYSTEM	-4.0	16.000	-0.2	OPEN F	86.3F
200	0.0	0.0	0.0	0.0	0.0	0.0	0.2	SYSTEM	-4.0	16.000	0.2	OPEN F	86.7F
300	1.9	5.0	5.0	5.0	5.0	5.0	0.6	SYSTEM	-3.6	16.000	2.0	OPEN F	85.4F
15:13:50	-1.3	0.4	0.4	0.4	0.4	0.4	0.2	SYSTEM	-4.0	16.000	0.8	OPEN F	86.5F
200	-1.0	0.7	0.7	0.7	0.7	0.7	0.2	SYSTEM	-4.0	16.000	0.8	OPEN F	87.0F
300	1.9	5.8	5.8	5.8	5.8	5.8	0.6	SYSTEM	-3.6	16.000	2.0	OPEN F	85.5F
15:17:09	7.5	0.0	0.0	0.0	0.0	0.0	0.5	SYSTEM	-4.0	16.000	0.8	OPEN F	84.4F
200	2.0	0.0	0.0	0.0	0.0	0.0	0.5	SYSTEM	-4.0	16.000	0.8	OPEN F	84.2F
300	7.5	5.8	5.8	5.8	5.8	5.8	1.0	SYSTEM	-3.6	16.000	2.0	OPEN F	85.5F
15:17:47	7.5	0.0	0.0	0.0	0.0	0.0	0.4	SYSTEM	-4.0	16.000	0.9	OPEN F	86.0F
200	2.0	0.0	0.0	0.0	0.0	0.0	0.4	SYSTEM	-4.0	16.000	0.8	OPEN F	85.6F
300	7.5	5.8	5.8	5.8	5.8	5.8	1.0	SYSTEM	-3.6	16.000	2.0	OPEN F	85.5F
15:19:15	5.2	0.0	0.0	0.0	0.0	0.0	0.4	SYSTEM	-4.0	4.0000	0.9	OPEN F	86.0F
200	2.3	0.0	0.0	0.0	0.0	0.0	0.4	SYSTEM	-4.0	4.0000	0.8	OPEN F	85.6F
300	5.2	5.0	5.0	5.0	5.0	5.0	1.1	SYSTEM	-3.7	4.0000	2.0	OPEN F	85.5F
15:20:00	0.0	18.1	18.1	18.1	18.1	18.1	0.2	SYSTEM	-4.0	16.000	0.6	OPEN F	86.0F
200	5.7	3.2	3.2	3.2	3.2	3.2	0.3	SYSTEM	-4.0	16.000	3.0	OPEN F	85.7F
300	2.3	4.9	4.9	4.9	4.9	4.9	1.0	SYSTEM	-3.8	16.000	1.9	OPEN F	85.6F
15:22:00	-0.3	21.4	21.4	21.4	21.4	21.4	0.2	SYSTEM	-4.0	16.000	0.5	OPEN F	86.7F
200	-0.2	20.9	20.9	20.9	20.9	20.9	0.2	SYSTEM	-4.0	16.000	0.4	OPEN F	86.0F
300	2.3	5.6	5.6	5.6	5.6	5.6	0.6	SYSTEM	-3.8	16.000	1.9	OPEN F	85.6F
15:24:00	-0.4	21.5	21.5	21.5	21.5	21.5	0.2	SYSTEM	-4.0	16.000	0.3	OPEN F	86.5F
200	-0.2	21.2	21.2	21.2	21.2	21.2	0.2	SYSTEM	-4.0	16.000	0.4	OPEN F	86.4F
300	2.1	6.3	6.3	6.3	6.3	6.3	0.6	SYSTEM	-3.8	16.000	1.9	OPEN F	85.7F

TRC ENVIRONMENTAL CONSULTANTS ALGONQUIN GAS TRANSMISSION COMPANY HANOVER NJ EMISSION COMPLIANCE PROGRAM

123	01	02	03	04	05	06	07	08	09	10	11	12	13	14	15	16
1114	CO	NO ₂	NO ₂	NO ₂	NO ₂	NO ₂	CO ₂	CO	CO	PPH	THC	STACK	TEMP	WELS	TEMP	
100	PPM	PERCENT	PERCENT	PPM	PPM	PPM	PERCENT	PPM	PPM	PPM	PPM	PPM	PPM	PPM	PPM	
15:26:00	-0.4	21.5	21.5	1.0	1.0	-4.0	0.2	-4.0	16.000	0.4	0.4	OPEN F	85.8			
200	-0.5	21.5	21.5	1.0	1.0	-4.0	0.2	-4.0	16.000	0.4	0.4	OPEN F	85.9			
300	1.8	7.0	7.0	29.7	29.7	-3.9	0.6	-3.9	1.8	1.8	1.8	WORLD	85.8			
15:28:00	-0.4	21.5	21.5	1.0	1.0	-4.0	0.2	-4.0	16.000	0.6	0.6	OPEN F	87.1F			
200	-0.4	21.5	21.5	1.0	1.0	-4.0	0.2	-4.0	16.000	0.4	0.4	OPEN F	86.3			
300	1.7	7.5	7.5	29.7	29.7	-3.9	0.5	-3.9	1.3	1.3	1.3	WORLD	85.8			
15:30:00	-0.4	21.5	21.5	1.0	1.0	-4.0	0.2	-4.0	16.000	1.5	1.5	OPEN F	87.5F			
200	-0.4	21.5	21.5	1.0	1.0	-4.0	0.2	-4.0	16.000	0.5	0.5	OPEN F	86.3			
300	1.7	7.5	7.5	29.7	29.7	-3.8	0.5	-3.8	0.9	0.9	0.9	WORLD	85.7			
15:32:00	-0.3	21.5	21.5	1.3	1.3	-4.0	0.2	-4.0	16.000	31.8	31.8	OPEN F	83.9F			
200	-0.3	21.5	21.5	1.1	1.1	-4.5	0.2	-4.5	13.2	13.2	13.2	OPEN F	83.3			
300	1.7	8.2	8.2	29.7	29.7	-3.8	0.6	-3.8	1.7	1.7	1.7	WORLD	85.7			
15:34:00	93.3	18.9	18.9	17.2	17.2	-4.0	1.7	-4.0	16.000	2.1	2.1	OPEN F	85.1F			
200	48.1	20.5	20.5	3.9	3.9	-4.3	0.8	-4.3	16.000	8.3	8.3	OPEN F	83.8			
300	4.8	8.9	8.9	30.3	30.3	-3.7	0.6	-3.7	1.7	1.7	1.7	WORLD	85.7			
15:36:00	16.9	18.0	18.0	33.8	33.8	-4.0	2.5	-4.0	16.000	0.0	0.0	OPEN F	86.6F			
200	31.5	18.3	18.3	26.0	26.0	-4.0	2.0	-4.0	16.000	0.0	0.0	OPEN F	86.6			
300	5.4	9.5	9.5	31.4	31.4	-3.7	0.7	-3.7	1.7	1.7	1.7	WORLD	85.7			
15:38:00	8.4	17.0	17.0	87.2	87.2	-4.0	2.7	-4.0	16.000	-0.2	-0.2	OPEN F	86.0F			
200	17.2	17.5	17.5	56.0	56.0	-4.1	2.4	-4.1	16.000	0.0	0.0	OPEN F	86.0			
300	5.6	10.0	10.0	34.3	34.3	-3.7	0.8	-3.7	1.7	1.7	1.7	WORLD	85.8			
15:40:00	7.6	17.1	17.1	85.2	85.2	-4.0	2.6	-4.0	16.000	-0.3	-0.3	OPEN F	86.5F			
200	13.6	17.3	17.3	68.2	68.2	-4.0	2.5	-4.0	16.000	-0.1	-0.1	OPEN F	86.5			
300	5.9	10.6	10.6	32.7	32.7	-3.8	0.9	-3.8	1.7	1.7	1.7	WORLD	85.8			
15:42:00	7.6	17.1	17.1	84.5	84.5	-4.0	2.6	-4.0	16.000	-0.4	-0.4	OPEN F	86.0F			
200	7.8	17.1	17.1	84.5	84.5	-4.0	2.6	-4.0	16.000	-0.3	-0.3	OPEN F	86.1			
300	6.1	11.2	11.2	30.7	30.7	-3.8	0.9	-3.8	1.7	1.7	1.7	WORLD	85.8			
15:44:00	7.7	17.1	17.1	83.8	83.8	-6.0	2.6	-6.0	36.000	-0.3	-0.3	OPEN F	86.4F			
200	7.8	17.1	17.1	84.3	84.3	-4.1	2.6	-4.1	36.000	-0.2	-0.2	OPEN F	86.3			
300	6.4	11.2	11.2	28.8	28.8	-4.0	1.0	-4.0	1.7	1.7	1.7	WORLD	85.9			

TEST 1-3 11/14/90 1540

PAGE 4

TRC ENVIRONMENTAL CONSULTANTS ALGONQUIN GAS TRANSMISSION COMPANY HANOVER NJ EMISSION COMPLIANCE PROGRAM

123	TRC ENVIRONMENTAL CONSULTANTS	ALGONQUIN GAS TRANSMISSION COMPANY	HANDOVER, NJ	EMISSION CAPABILITY: PPM/PPH																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																						
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CEM Part 3

Scott Specialty Gases



Electronics Group

2330 Hamilton Blvd., South Plainfield, N.J. 07080

Phone: (201) 754-7700 FAX: (201) 754-7303



SCOTT SPECIALTY GASES, INC.

4/27/90

CERTIFICATE OF ANALYSIS

TRC
11 VILLAGE STREET
EAST HARTFORD

PROJECT #: 07-05450
PO #: 19646

CT 06108-0000

ATT:RECEIVING DEPT

CYLINDER #: 3L1716

ANALYTICAL ACCURACY: +/- 1%

COMPONENT	REQUESTED CONCENTRATION	ANALYSIS 1 (MOLES) U/M
PROPANE	10.0 PPM	9.67 PPM
AIR	BALANCE GAS	N/A

DATE OF ANALYSIS: 4/25/90

ANALYST: _____

ADELA SY

APPROVED BY: _____

JOHN O'SHEA

Mike Martin

Scott Specialty Gases



Electronics Group

2330 Hamilton Blvd., South Plainfield, N.J. 07080

Phone: (201) 754-7700 FAX: (201) 754-7303

SCOTT SPECIALTY GASES, INC.

4/27/90

CERTIFICATE OF ANALYSIS

TRC
11 VILLAGE STREET
EAST HARTFORD

PROJECT #: 07-05450
PG #: 19646

CT 06108-0000

ATT:RECEIVING DEPT

CYLINDER #: AAL8734

ANALYTICAL ACCURACY: +/- 1%

COMPONENT

REQUESTED
CONCENTRATION

ANALYSIS :
(MOLES) U/M

PROPANE
AIR

100.0 PPM
BALANCE GAS

104.0 PPM
N/A

DATE OF ANALYSIS: 4/25/90

ANALYST: _____

ADELA SY

APPROVED BY: _____

JOHN O'SHEA



Scott Specialty Gases

a division of
Scott Environmental Technology, Inc.

SOUTH PLAINFIELD, NJ 07080 PHONE: (201) 754-7700 TWX: 201844552

2772

TRC Environmental Consultants
11 Village Street
E. Hartford, CT 06108

Date: June 9, 1988

QC No.: F-098 JOA

Your P.O. No.: 17608

Invoice No.: 199789

ANALYTICAL REPORT

Cyl No. <u>AAL-2233</u> <u>AAL-6429</u>	Analytical Accuracy $\pm 1\%$
Component	Concentration
Carbon Monoxide	495 PPM
Nitrogen	Balance

Cyl No. <u>AAL-1746</u>	Analytical Accuracy $\pm 1\%$
Component	Concentration
Nitric Oxide	513 PPM
Nitrogen	Balance

Cyl No. <u>AAL-4033</u>	Analytical Accuracy $\pm 1\%$
Component	Concentration
Nitric Oxide	518 PPM
Nitrogen	Balance

Cyl No. <u>AAL-3934</u>	Analytical Accuracy
Component	Concentration
Sulfur Dioxide	239 PPM
Carbon Dioxide	12.0%
Nitrogen	Balance
ANALYTICAL ACCURACY	
Sulfur Dioxide	$\pm 1\%$
Carbon Dioxide	$\pm 0.02\%$ Absolute

Analyst John O'Shea

Approved By Adela Sy

RESULTS ARE IN VOLUME PERCENT UNLESS OTHERWISE INDICATED.

The only liability of this Company for gas which fails to comply with this analysis shall be replacement thereof by the Company without extra cost.

CERTIFIED REFERENCE MATERIALS EPA PROTOCOL GASES
ACUBLEND® CALIBRATION & SPECIALTY GAS MIXTURES PURE GASES
ACCESSORY PRODUCTS CUSTOM ANALYTICAL SERVICES

PLUMSTEADVILLE, PENNSYLVANIA / TROY, MICHIGAN / SAN BERNARDINO, CALIFORNIA / HOUSTON, TEXAS
WHEELING, ILLINOIS / FREMONT, CALIFORNIA / WAKEFIELD, MASSACHUSETTS / LONGMONT, COLORADO

Scott Specialty Gases

Electronics Group

2330 Hamilton Blvd., South Plainfield, N.J. 07080

Phone: (201) 754-7700 FAX: (201) 754-7303

SCOTT SPECIALTY GASES, INC.

3/06/90

CERTIFICATE OF ANALYSIS

TRC
11 VILLAGE STREET
EAST HARTFORD

PROJECT #: 07-04737
PO #: 19432

ATT:RECEIVING DEPT

CT 0610B-0000

CYLINDER #: ALM009709

ANALYTICAL ACCURACY: -

COMPONENT

REQUESTED
CONCENTRATION

ANALYSIS 1
(MOLES) U/M

CARBON DIOXIDE
SULFUR DIOXIDE
NITROGEN

5.0 PCT
100.0 PPM
BALANCE GAS

4.99 PCT
103.0 PPM
N/A

NOTES: THIS MATERIAL TRACEABLE TO NBS CRM 1675, CRM 1694

DATE OF ANALYSIS: 2/22/90

ANALYST: John O'Shea
JOHN O'SHEA

APPROVED BY: Donald Dudics
DONALD DUDICS

THE ONLY LIABILITY OF THIS COMPANY FOR GAS WHICH FAILS TO COMPLY WITH THIS
ANALYSIS SHALL BE THE REPLACEMENT THEREOF BY THE COMPANY WITHOUT EXTRA COST

APPENDIX C

EPA Method 20 Performance Checks



Electronics Group

2330 Hamilton Blvd., South Plainfield, N.J. 07080 Phone: (201) 754-7700 FAX: (201) 754-7303

Date Shipped 11/8/90
 Our Project No: 0707921
 Your P.O. No: 20262
 Page 2 of 2
 Expiration Date: 5/8/92

CERTIFICATE OF ANALYSIS—EPA PROTOCOL GASES*

Certified Per Traceability Protocol No. 1 Procedure No. G1 Cylinder No. ALM008205 Cylinder Pressure 2000 psig Certified Accuracy ± 1 % NBS Traceable

REFERENCE STD

COMPONENTS	CERTIFIED CONC	SRM/CRM NO.	CYL. NO.	CONC.
Nitric Oxide	143 ppm	1685	CAL5851	236 ppm

GAS ANALYZER

MAKE/MODEL/SERIAL NO.	LAST CAL. DATE	ANALYTICAL PRINCIPLE
Teco 10S/26404-225	8/15/90	Chemiluminescence

BALANCE GAS Nitrogen/Oxygen Free

ANALYZER READINGS: Z = Zero Gas T = Test Gas R = Reference Gas

Component	Nitric Oxide	10/31/90	Units	ppm
First Analysis Date		204	T	142
Z	204	R		
R		Z		142
Z	0	T		204
		R		142
Mean Test Assay				142
Second Analysis Date	11/8/90	Units	ppm	
Z	204	R	T	143
R		Z	T	143
Z	0	T	R	204
Mean Test Assay				143

Component	Date	Units	Mean Test Assay
Z		R	T
R		Z	T
Z		T	R
Mean Test Assay			
Date		Units	
Z		R	T
R		Z	T
Z		T	R
Mean Test Assay			

Component	Date	Units	Mean Test Assay
Z		R	T
R		Z	T
Z		T	R
Mean Test Assay			
Date		Units	
Z		R	T
R		Z	T
Z		T	R
Mean Test Assay			

Analyst

John O'Shea

Approved By:

Adela Sy



Electronics Group

2330 Hamilton Blvd., South Plainfield, N.J. 07080

Phone: (201) 754-7700 FAX: (201) 754-7303

Date Shipped 11/8/90

Our Project No: 0707921

Your P.O. No: 20262

Page 1 of 2

Expiration Date: 5/8/92

CERTIFICATE OF ANALYSIS—EPA PROTOCOL GASES*

Certified Per Traceability Protocol No. 1 Procedure No. G1

Cylinder No. 1L2066

Cylinder Pressure 2000 psig

Certified Accuracy ± 1 % NBS Traceable

REFERENCE STD

COMPONENTS	CERTIFIED CONC	SRM/CRM NO.	CYL NO.	CONC.
Nitric Oxide	71.2 ppm	1684	ALM3675	97.28 ppm

GAS ANALYZER

MAKE/MODEL/SERIAL NO.	LAST CAL. DATE	ANALYTICAL PRINCIPLE
Teco 10S/26404-225	8/15/90	Chemiluminescence

BALANCE GAS Nitrogen/Oxygen Free

ANALYZER READINGS: Z = Zero Gas T = Test Gas R = Reference Gas

Component	Nitric Oxide	10/31/90	Units	ppm
First Analysis Date	0	R	97.28	T 70.7
	97.28	Z	0	T 70.7
	0	T	71.2	R 97.28
				R 70.9
Mean Test Assay	11/8/90			ppm
Second Analysis Date	0	R	97.28	T 71.4
	97.28	Z	0	T 71.4
	0	T	71.6	R 97.28
				R 71.5
Mean Test Assay				

Component	Date	Units	Mean Test Assay
Z		R	
R		Z	
Z		T	
			Mean Test Assay
Date		Units	
Z		R	
R		Z	
Z		T	
			Mean Test Assay

Analyst *John O'Shea*

Approved By: *Adela Sy*



Scott Specialty Gases

a division of
Scott Environmental Technology, Inc.

PLUMSTEADVILLE, PA 18949

PHONE: 215-766-8861

TWX: 510-665-9344

Shipped From: Scott So. Plainfield
Date Shipped 3/7/90
Our Project No: 0704737
Your P.O. No: 19432
Page 1 of 1
Expiration Date: 9/7/91

CERTIFICATE OF ANALYSIS - EPA PROTOCOL GASES*

Certified Per Traceability Protocol No. 1 Procedure No. G1

Cylinder No. ALM-005152

Cylinder Pressure 2000 psig

Certified Accuracy ± 1 % NBS Traceable

REFERENCE STD

COMPONENTS	CERTIFIED CONC	SRM/CRM NO.	CYL. NO.	CONC.
Oxygen	22.06%	2659	AAL-18592	20.66%

GAS ANALYZER

MAKEMODEL/SERIAL NO.	LAST CAL. DATE	ANALYTICAL PRINCIPLE
Varian 3700	2/2/90	GC - TCD
372000-00/31608928-11		

BALANCE GAS Nitrogen

ANALYZER READINGS: Z = Zero Gas T = Test Gas R = Reference Gas

Component	Oxygen	3/7/90	Units	Z
First Analysis Date				
Z	0	R 20.66	T 22.06	
R	20.66	Z 0	T 22.02	
Z	0	T 22.10	R 20.66	
Mean Test Assay			22.06	

Second Analysis Date	Units	Mean Test Assay
Z	R	T
R	Z	T
Z	T	R
Mean Test Assay		

Component	Date	Units	Mean Test Assay
Z	R	T	
R	Z	T	
Z	T	R	
Mean Test Assay			

Date	Units	Mean Test Assay
Z	R	T
R	Z	T
Z	T	R
Mean Test Assay		

Chronology: Date 3/7/90
Assay 20.06% O2

Analyst John O'Shea

Approved By: Adela Sy

SCOTT Specialty Gases



Electronics Group

2772

2330 Hamilton Blvd., South Plainfield, N.J. 07080

Phone: (201) 754-7700 FAX: (201) 754-7303

TRC ENVIRONMENTAL CONSULTANTS
11 VILLAGE STREET
E.HARTFORD CT 06108

Date: January 19, 1989

QC No.: A-199 AAS

Your P.O. No.: 18272

Invoice No.: 122962

ANALYTICAL REPORT

Cyl No. <u>ALM-2023</u>	Analytical Accuracy _____
Component	Concentration
NITROGEN-ZERO	99.998%MIN.
THC	LT 0.5PPM

Cyl No. <u>ALM-2120</u>	Analytical Accuracy _____
Component	Concentration
AIR	ZERO
THC	LT 0.5PPM

Cyl No. <u>ALM-2015</u>	Analytical Accuracy _____
Component	Concentration
AIR	ZERO
THC	LT 0.5PPM

Cyl No. _____	Analytical Accuracy _____
Component	Concentration

Analyst

Adela Sy

Approved By

John O'Shea

RESULTS ARE IN VOLUME PERCENT UNLESS OTHERWISE INDICATED.

The only liability of this Company for gas which fails to comply with this analysis shall be replacement thereof by the Company without extra cost.

CERTIFIED REFERENCE MATERIALS EPA PROTOCOL GASES
ACUBLEND® CALIBRATION & SPECIALTY GAS MIXTURES PURE GASES
ACCESSORY PRODUCTS CUSTOM ANALYTICAL SERVICES

PLUMSTEADVILLE, PENNSYLVANIA / TROY, MICHIGAN / SAN BERNARDINO, CALIFORNIA / HOUSTON, TEXAS
WHEELING, ILLINOIS / FREMONT, CALIFORNIA / WAKEFIELD, MASSACHUSETTS / LONGMONT, COLORADO

TURBINE SAMPLING SYSTEM

Zero and Span Drift Data

Turbine Type Simple cycle LNB S/N CC84068

Date: 11/13/90

Test No.: T-1-1

Analyzer: Type NO_x (Thermo Electron) S/N 10AR22558205

	Initial Calibration, <u>ppm</u> or %	Final Calibration, <u>ppm</u> or %	Difference Initial-Final, <u>ppm</u> or %	% of Span
Zero Gas	0.2	-0.7	0.9	0.4
High Calibration Gas (Span Gas)	146.0	145.7	0.3 *	0.1

$$\% \text{ of Span} = \frac{\text{Absolute Value of Difference}}{\text{Instrument Span}} \times 100$$

* Corrected for zero drift, i.e., if zero drift over test period is +2 ppm then 2 ppm shall be subtracted from the difference between the initial and final readings.

EPA METHOD 20 TURBINE SAMPLING SYSTEM

Zero and Span Calibration Data

Turbine Simple cycle #1 (LNB) Identification number 0001

Date: 11/13/90 Test Number T-1-1

Analyzer type: NO_x Thermo Electron Identification number 10AR22558205

	Cylinder value, <u>ppm</u> or %	Initial analyzer response, <u>ppm</u> or %	Final analyzer responses, <u>ppm</u> or %	Difference: initial-final, <u>ppm</u> or %	
Zero gas	0.0	0.0	-0.7	0.7	0.3
Low - level gas	71.2	72.2	74.2	2.0	0.8
Mid - level gas	143.0	147.5	145.7	1.8	0.7
High - level gas					

$$\text{Percent drift} = \frac{\text{Absolute Difference}}{\text{Span value}} \times 100$$

EPA METHOD 20
TURBINE SAMPLING SYSTEM

Zero and Span Drift Data

Turbine Type LNG Simple Cycle turbine #2 S/N CC84067
 Date: 11/14/90
 Test No.: Tests # 1, 2, 3
 Analyzer: Type Nox Thermoelectron S/N 10AR22558205

	Initial Calibration, ppm or %	Final Calibration, ppm or %	Difference Initial-Final, ppm or %	% of Span
Zero Gas	0.0	-0.2	0.2	0.08
High Calibration Gas (Span Gas)	142.7	142.8 153.0	0.1 * 12.3	4.1 0.04

$$\% \text{ of Span} = \frac{\text{Absolute Value of Difference}}{\text{Instrument Span}} \times 100$$

- * Corrected for zero drift, i.e., if zero drift over test period is +2 ppm then 2 ppm shall be subtracted from the difference between the initial and final readings.

EPA METHOD 20
TURBINE SAMPLING SYSTEM

Zero and Span Calibration Data

Turbine LNG Simple Cycle #2 Identification number 0002
 Date: 11/14/90 Test Number Tests 1, 2, 3
 Analyzer type: Thermoelectron Nox Identification number 10AR22558205

	Cylinder value, ppm or %	Initial analyzer response, ppm or %	Final analyzer responses, ppm or %	Difference: initial-final, ppm or %
Zero gas	0.0	-0.2	-0.2	0.08 0.0
Low - level gas	71.7	73.8	74.0	0.2
Mid - level gas	143	142.7	153.0 142.8	11.0 0.1
High - level gas				

$$\text{Percent drift} = \frac{\text{Absolute Difference}}{\text{Span value}} \times 100$$

TRC ENVIRONMENTAL CONSULTANTS ALGONQUIN GAS TRANSMISSION COMPANY HARDYER NJ EMISSION COMPLIANCE PROGRAM

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0.0 ZERO ANALYZER

0.0 ZERO RACK

143.5 MID SPAN 143.0 PPM

147.5 MID SPAN

101.7 LOW SPAN

11.7 MID RACK

22.4 22.0 SPAN UPPER

5.4 CO2 MID 570

12.7 CO2 UPPER 1270

INTERFERENCE CHECK

11/13

TRC ENVIRONMENTAL CONSULTANTS				ALGONQUIN GAS TRANSMISSION COMPANY				HANOVER NJ EMISSION COMPLIANCE PROGRAM							
01	02	03	04	05	06	07	08	09	10	11	12	13	14	15	16
CO		OXYGEN		NOX		CO2		CO		THC		TEMP	STACK	MFIS	
PPM		PERCENT		PPM		PERCENT		PPM		PPM				TEMP	
2:47	ANALYZER ZERO	21.6 21.6 21.6	ANALYZER ZERO	0.2 0.2 0.3	0.1 0.1 0.1	0.1 0.1 0.1	0.1 0.1 0.1	-4.0 -3.5 -3.0	16.000	0.1 0.0 0.1	ANALYZER ZERO	PPEN F PPEN MURLD	80.0F 79.7 81.6		
6:51	RACK ZERO	0.1 0.1 20.8	RACK ZERO	0.0 0.0 0.3	0.1 0.1 0.1	0.1 0.1 0.1	0.1 0.1 0.1	-4.0 -4.0 -3.0	16.000	0.0 0.0 0.1	ANALYZER ZERO	PPEN F PPEN MURLD	80.3F 80.3 81.4		
5:37		0.1 0.2 -1.0		142.7 141.6 13.2	0.1 0.1 0.1	0.1 0.1 0.1	0.1 0.1 0.1	-4.0 -4.0 -3.2	16.000	0.1 0.1 0.1		PPEN F PPEN MURLD	80.1F 79.4 81.2		
9:48		0.3 0.0 -0.9		73.8 111.8 20.6	0.1 0.1 0.1	0.1 0.1 0.1	0.1 0.1 0.1	-4.0 -4.0 -3.1	16.000	1.2 0.5 0.1	ANALYZER ZERO	PPEN F PPEN MURLD	81.1F 80.4 81.1		
11:34		-0.2 0.2 -0.9		73.0 73.9 23.0	0.1 0.1 0.1	0.1 0.1 0.1	0.1 0.1 0.1	-4.0 -4.0 -3.2	16.000	0.2 0.5 0.1	ANALYZER ZERO	PPEN F PPEN MURLD	79.7F 79.6 81.1		
46:09		0.0 0.0 -0.7		0.2 25.7	0.1 0.1	0.1 0.1	0.1 0.1	-4.0 -3.2	16.000	0.7 0.7	SPAD	PPEN F PPEN MURLD	80.6F 80.8 80.8		
49:35		0.2 0.1 -0.7		0.2 0.2 25.6	0.1 0.1 0.1	0.1 0.1 0.1	0.1 0.1 0.1	-4.0 -4.0 -3.3	16.000	3.9 5.3 0.8	ANALYZER ZERO	PPEN F PPEN MURLD	81.2F 80.8 80.8		
52:21		0.2 0.2 -0.6		0.2 0.1 25.6	0.1 0.1 0.1	0.1 0.1 0.1	0.1 0.1 0.1	-4.0 -4.0 -3.4	16.000	4.7 2.5 1.1	ANALYZER ZERO	PPEN F PPEN MURLD	81.1F 80.9 80.7		
55:00		0.9 1.6 -0.5		0.2 0.4 25.6	0.1 0.1 0.1	0.1 0.1 0.1	0.1 0.1 0.1	-4.0 -4.0 -3.4	16.000	4.5 4.5 1.4	SPAD	PPEN F PPEN MURLD	80.2F 80.3 80.6		
58:11		1.9 1.4 -0.4		0.2 0.3 25.6	0.1 0.1 0.1	0.1 0.1 0.1	0.1 0.1 0.1	-4.0 -4.0 -3.5	16.000	-1.0 3.9 1.3	ANALYZER ZERO	PPEN F PPEN MURLD	80.2F 80.5 80.6		

EPA METHOD 20

RESPONSE TIME *System*Date of Test 11/13/90 S/N _____Analyzer Type Thermo Electron Nox Model 10Span Gas Concentration 143 ppmAnalyzer Span Setting ~~146~~ 137.2 ppm *System*1 130 secondsUpscale 2 132 seconds3 130 secondsAverage upscale response 131 seconds1 105 secondsDownscale 2 120 seconds3 118 secondsAverage downscale response 114 secondsSystem response time = slower average time = 131 seconds.Date of Test 11/14/90 S/N _____Analyzer Type Nox Thermo Electron Model 10Span Gas Concentration 143 ppmAnalyzer Span Setting 142.7 ppm1 131 secondsUpscale 2 130 seconds3 142 secondsAverage upscale response 134 seconds1 120 secondsDownscale 2 117 seconds3 128 secondsAverage downscale response 120 secondsSystem response time = slower average time = 134 seconds.

APPENDIX D
Process Data

41 Unit
7/13/90

11:30 AM

GT - HANOVER COMPRESSOR STATION
POLAR CENTAUR 3830 NATURAL GAS TURBINE/COMPRESSOR PERFORMANCE
DATE 14:25:24 TIME 11-13-1990

OPERATING CONDITIONS

INLET PRESSURE	593 PSIG	FUEL FLOW	40 MMBTU/H
DISCHARGE PRESSURE	665 PSIG	PCD	122 PSIG
PRESSURE RATIO	1.12	T5	1090 DEG F
INLET TEMPERATURE	61 DEG F	NGP	100 %
DISCHARGE TEMPERATURE	85 DEG F	NPT	91 %
THROUGHPUT	25190 MMBTU/H	FUEL RATIO	0.2 % FUEL/THROUGHPUT
AMBIENT TEMPERATURE	39 DEG F		

PERFORMANCE PARAMETERS

	GROSS HP BEFORE LOSSES	INLET LOSSES HP	EXHAUST LOSSES HP	NPT LOSSES HP	ELEV. LOSSES HP	NET HP AFTER LOSSES
FUEL	15545					
RATED	4006	31	20	18	-10	3947
NGP	4010	31	20	18	-10	3950
PCD	3900	31	20	12	-9	3846
5	4056	32	20	20	-10	3994
COMP	2724					

	% EFF	
RATED	25.4	RATED NET HP/FUEL GROSS HP
NGP	100.1	NET NGP HP/NET RATED HP
PCD	97.4	NET PCD HP/NET RATED HP
5	101.2	NET T5 HP/NET RATED HP
COMP	69.3	COMPRESSOR HP/AVERAGE NET HP
OVERALL	17.5	COMPRESSOR HP/FUEL HP

#1 Unit

- 11/13/90

12:00 Noon

GT - HANOVER COMPRESSOR STATION
 SOLAR CENTAUR 3830 NATURAL GAS TURBINE/COMPRESSOR PERFORMANCE
 DATE 14:43:19 TIME 11-13-1990

OPERATING CONDITIONS

INLET PRESSURE	611 PSIG	FUEL FLOW	40 MMBTU/H
DISCHARGE PRESSURE	672 PSIG	PCD	121 PSIG
PRESSURE RATIO	1.10	T5	1090 DEG F
INLET TEMPERATURE	70 DEG F	NGP	100 %
DISCHARGE TEMPERATURE	90 DEG F	NPT	89 %
THROUGHPUT	27822 MMBTU/H	FUEL RATIO	0.1 % FUEL/THROUGHPUT
AMBIENT TEMPERATURE	40 DEG F		

PERFORMANCE PARAMETERS

	GROSS HP BEFORE LOSSES	INLET LOSSES HP	EXHAUST LOSSES HP	NPT LOSSES HP	ELEV. LOSSES HP	NET HP AFTER LOSSES
FUEL	15545					
RATED	3998	31	20	30	-9	3926
NGP	4001	31	20	31	-9	3929
PCD	3839	30	19	20	-9	3777
5	4040	32	20	33	-10	3965
COMP	2545					

	% EFF	
RATED	25.3	RATED NET HP/FUEL GROSS HP
NGP	100.1	NET NGP HP/NET RATED HP
CD	96.2	NET PCD HP/NET RATED HP
5	101.0	NET T5 HP/NET RATED HP
COMP	65.4	COMPRESSOR HP/AVERAGE NET HP
OVERALL	16.4	COMPRESSOR HP/FUEL HP

#1 Unit

11/13/90

1:00 PM

GT - HANOVER COMPRESSOR STATION
 SOLAR CENTAUR 3830 NATURAL GAS TURBINE/COMPRESSOR PERFORMANCE
 DATE 14:40:35 TIME 11-13-1990

OPERATING CONDITIONS

INLET PRESSURE	622 PSIG	FUEL FLOW	40 MMBTU/H
DISCHARGE PRESSURE	672 PSIG	PCD	122 PSIG
PRESSURE RATIO	1.08	T5	1090 DEG F
INLET TEMPERATURE	74 DEG F	NGP	100 %
DISCHARGE TEMPERATURE	94 DEG F	NPT	88 %
THROUGHPUT	29232 MMBTU/H	FUEL RATIO	0.1 % FUEL/THROUGHPUT
AMBIENT TEMPERATURE	40 DEG F		

PERFORMANCE PARAMETERS

	GROSS HP BEFORE LOSSES	INLET LOSSES HP	EXHAUST LOSSES HP	NPT LOSSES HP	ELEV. LOSSES HP	NET HP AFTER LOSSES
FUEL	15545					
RATED	3998	31	20	38	-9	3918
NGP	4001	31	20	38	-9	3921
CD	3902	31	20	31	-9	3830
5	4040	32	20	41	-10	3956
COMP	2187					
	% EFF					
RATED	25.2	RATED NET HP/FUEL GROSS HP				
NGP	100.1	NET NGP HP/NET RATED HP				
CD	97.8	NET PCD HP/NET RATED HP				
5	101.0	NET T5 HP/NET RATED HP				
COMP	56.1	COMPRESSOR HP/AVERAGE NET HP				
VERALL	14.1	COMPRESSOR HP/FUEL HP				

#1 Unit

2:00 PM

7/13/90

AGT - HANOVER COMPRESSOR STATION

SOLAR CENTAUR 3830 NATURAL GAS TURBINE/COMPRESSOR PERFORMANCE

DATE 14:46:08 TIME 11-13-1990

OPERATING CONDITIONS

SUCTION PRESSURE	652 PSIG	FUEL FLOW	40 MMBTU/H
DISCHARGE PRESSURE	671 PSIG	PCD	121 PSIG
PRESSURE RATIO	1.03	T5	1090 DEG F
SUCTION TEMPERATURE	85 DEG F	NGP	100 %
DISCHARGE TEMPERATURE	111 DEG F	NPT	89 %
THROUGHPUT	12495 MMBTU/H	FUEL RATIO	0.3 % FUEL/THROUGHPUT
AMBIENT TEMPERATURE	41 DEG F		

PERFORMANCE PARAMETERS

	GROSS HP BEFORE LOSSES	INLET LOSSES HP	EXHAUST LOSSES HP	NPT LOSSES HP	ELEV. LOSSES HP	NET HP AFTER LOSSES
FUEL	15545					
RATED	3990	31	20	30	-9	3918
NGP	3993	31	20	30	-9	3921
PCD	3841	30	19	21	-9	3780
T5	4024	31	20	32	-10	3949
COMP	354					
% EFF						
RATED	25.2	RATED NET HP/FUEL GROSS HP				
NGP	100.1	NET NGP HP/NET RATED HP				
PCD	96.5	NET PCD HP/NET RATED HP				
T5	100.8	NET T5 HP/NET RATED HP				
COMP	9.1	COMPRESSOR HP/AVERAGE NET HP				
OVERALL	2.3	COMPRESSOR HP/FUEL HP				

#1 Unit

3:00 PM

11/13/90

AGT - HANOVER COMPRESSOR STATION

SOLAR CENTAUR 3830 NATURAL GAS TURBINE/COMPRESSOR PERFORMANCE

DATE 15:03:14 TIME 11-13-1990

OPERATING CONDITIONS

SUCTION PRESSURE	663 PSIG	FUEL FLOW	30 MMBTU/H
DISCHARGE PRESSURE	676 PSIG	PCD	82 PSIG
PRESSURE RATIO	1.02	T5	800 DEG F
SUCTION TEMPERATURE	86 DEG F	NGP	84 %
DISCHARGE TEMPERATURE	103 DEG F	NPT	64 %
THROUGHPUT	12529 MMBTU/H	FUEL RATIO	0.2 % FUEL/THROUGHPUT
AMBIENT TEMPERATURE	41 DEG F		

PERFORMANCE PARAMETERS

	GROSS HP BEFORE LOSSES	INLET LOSSES HP	EXHAUST LOSSES HP	NPT LOSSES HP	ELEV. LOSSES HP	NET HP AFTER LOSSES
--	---------------------------------	-----------------------	-------------------------	---------------------	-----------------------	------------------------------

FUEL	11853					
RATED	3990	31	20	408	-9	3486
NGP	1977	19	14	60	-5	1887
CD	2199	21	15	66	-5	2100
5	1999	19	14	62	-5	1907
COMP	240					

% EFF

RATED	29.4	RATED NET HP/FUEL GROSS HP
NGP	54.1	NET NGP HP/NET RATED HP
CD	60.2	NET PCD HP/NET RATED HP
T5	54.7	NET T5 HP/NET RATED HP
COMP	12.2	COMPRESSOR HP/AVERAGE NET HP
VERALL	2.0	COMPRESSOR HP/FUEL HP

1 Unit
7/13/90

3:25 PM

AGT - HANOVER COMPRESSOR STATION
SOLAR CENTAUR 3830 NATURAL GAS TURBINE/COMPRESSOR PERFORMANCE
DATE 15:45:25 TIME 11-13-1990

OPERATING CONDITIONS

SUCTION PRESSURE	663 PSIG	FUEL FLOW	28 MMBTU/H
DISCHARGE PRESSURE	675 PSIG	PCD	77 PSIG
PRESSURE RATIO	1.02	T5	780 DEG F
SUCTION TEMPERATURE	79 DEG F	NGP	83 %
DISCHARGE TEMPERATURE	94 DEG F	NPT	61 %
THROUGHPUT	12627 MMBTU/H	FUEL RATIO	0.2 % FUEL/THROUGHPUT
AMBIENT TEMPERATURE	41 DEG F		

PERFORMANCE PARAMETERS

	GROSS HP BEFORE LOSSES	INLET LOSSES HP	EXHAUST LOSSES HP	NPT LOSSES HP	ELEV. LOSSES HP	NET HP AFTER LOSSES
FUEL	11180					
RATED	3990	31	20	475	-9	3396
NGP	1851	18	13	74	-4	1747
CD	0	0	0	0	0	0
T5	1853	18	13	74	-4	1748
COMP	219					

	% EFF	
RATED	30.4	RATED NET HP/FUEL GROSS HP
NGP	51.5	NET NGP HP/NET RATED HP
CD	0.0	NET PCD HP/NET RATED HP
T5	51.5	NET T5 HP/NET RATED HP
COMP	18.8	COMPRESSOR HP/AVERAGE NET HP
VERALL	2.0	COMPRESSOR HP/FUEL HP

#1 Turbine

11/14/90

3:40 PM

GT - HANOVER COMPRESSOR STATION
SOLAR CENTAUR 3830 NATURAL GAS TURBINE/COMPRESSOR PERFORMANCE
DATE 17:47:21 TIME 11-14-1990

OPERATING CONDITIONS

INLET PRESSURE	610 PSIG	FUEL FLOW	40 MMBTU/H
DISCHARGE PRESSURE	657 PSIG	PCD	122 PSIG
PRESSURE RATIO	1.08	T5	1100 DEG F
INLET TEMPERATURE	69 DEG F	NGP	100 %
DISCHARGE TEMPERATURE	87 DEG F	NPT	86 %
THROUGHPUT	29903 MMBTU/H	FUEL RATIO	0.1 % FUEL/THROUGHPUT
AMBIENT TEMPERATURE	47 DEG F		

PERFORMANCE PARAMETERS

	GROSS HP BEFORE LOSSES	INLET LOSSES HP	EXHAUST LOSSES HP	NPT LOSSES HP	ELEV. LOSSES HP	NET HP AFTER LOSSES
FUEL	15813					
RATED	3940	31	20	54	-9	3844
NGP	3944	31	20	54	-9	3848
PCD	3922	31	20	52	-9	3828
5	3986	31	20	58	-9	3886
COMP	2123					
	% EFF	RATED NET HP/FUEL GROSS HP				
RATED	24.3	NET NGP HP/NET RATED HP				
NGP	100.1	NET PCD HP/NET RATED HP				
CD	99.6	NET T5 HP/NET RATED HP				
5	101.1	COMPRESSOR HP/AVERAGE NET HP				
COMP	55.1	COMPRESSOR HP/FUEL HP				
OVERALL	13.4					

#1 Turbine

11/14/90

4:30 PM

GT - HANOVER COMPRESSOR STATION
SOLAR CENTAUR 3830 NATURAL GAS TURBINE/COMPRESSOR PERFORMANCE
DATE 17:42:11 TIME 11-14-1990

OPERATING CONDITIONS

INLET PRESSURE	616 PSIG	FUEL FLOW	40 MMBTU/H
DISCHARGE PRESSURE	664 PSIG	PCD	122 PSIG
PRESSURE RATIO	1.08	T5	1090 DEG F
INLET TEMPERATURE	74 DEG F	NGP	100 %
DISCHARGE TEMPERATURE	93 DEG F	NPT	86 %
THROUGHPUT	29499 MMBTU/H	FUEL RATIO	0.1 % FUEL/THROUGHPUT
AMBIENT TEMPERATURE	46 DEG F		

PERFORMANCE PARAMETERS

	GROSS HP BEFORE LOSSES	INLET LOSSES HP	EXHAUST LOSSES HP	NPT LOSSES HP	ELEV. LOSSES HP	NET HP AFTER LOSSES
FUEL	15813					
RATED	3948	31	20	54	-9	3852
NGP	3952	31	20	54	-9	3856
PCD	3919	31	20	51	-9	3826
5	3943	31	20	53	-9	3847
COMP	2143					

	% EFF	
RATED	24.4	RATED NET HP/FUEL GROSS HP
NGP	100.1	NET NGP HP/NET RATED HP
CD	99.3	NET PCD HP/NET RATED HP
5	99.9	NET T5 HP/NET RATED HP
COMP	55.8	COMPRESSOR HP/AVERAGE NET HP
OVERALL	13.6	COMPRESSOR HP/FUEL HP

#1 Turbine

11/14/90

5:00 PM

GT - HANOVER COMPRESSOR STATION
SOLAR CENTAUR 3830 NATURAL GAS TURBINE/COMPRESSOR PERFORMANCE
DATE 17:43:48 TIME 11-14-1990

OPERATING CONDITIONS

INLET PRESSURE	619 PSIG	FUEL FLOW	41 MMBTU/H
DISCHARGE PRESSURE	670 PSIG	PCD	122 PSIG
PRESSURE RATIO	1.08	T5	1090 DEG F
INLET TEMPERATURE	74 DEG F	NGP	100 %
DISCHARGE TEMPERATURE	94 DEG F	NPT	86 %
THROUGHPUT	29640 MMBTU/H	FUEL RATIO	0.1 % FUEL/THROUGHPUT
AMBIENT TEMPERATURE	44 DEG F		

PERFORMANCE PARAMETERS

	GROSS HP BEFORE LOSSES	INLET LOSSES HP	EXHAUST LOSSES HP	NPT LOSSES HP	ELEV. LOSSES HP	NET HP AFTER LOSSES
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FUEL	16081					
RATED	3965	31	20	55	-9	3868
NGP	3969	31	20	55	-9	3871
PCD	3914	31	20	50	-9	3822
5	3975	31	20	56	-9	3877
COMP	2273					

% EFF

RATED	24.1	RATED NET HP/FUEL GROSS HP
NGP	100.1	NET NGP HP/NET RATED HP
CD	98.8	NET PCD HP/NET RATED HP
5	100.2	NET T5 HP/NET RATED HP
COMP	58.9	COMPRESSOR HP/AVERAGE NET HP
OVERALL	14.1	COMPRESSOR HP/FUEL HP

#2 Turbine

7:15 AM

11/14/90

GT - HANOVER COMPRESSOR STATION

POLAR CENTAUR 3830 NATURAL GAS TURBINE/COMPRESSOR PERFORMANCE

DATE 08:21:38 TIME 11-14-1990

OPERATING CONDITIONS

INLET PRESSURE	617 PSIG	FUEL FLOW	41 MMBTU/H
DISCHARGE PRESSURE	670 PSIG	PCD	124 PSIG
PRESSURE RATIO	1.08	T5	1090 DEG F
INLET TEMPERATURE	72 DEG F	NGP	100 %
DISCHARGE TEMPERATURE	89 DEG F	NPT	87 %
THROUGHPUT	30672 MMBTU/H	FUEL RATIO	0.1 % FUEL/THROUGHPUT
AMBIENT TEMPERATURE	33 DEG F		

PERFORMANCE PARAMETERS

	GROSS HP BEFORE LOSSES	INLET LOSSES HP	EXHAUST LOSSES HP	NPT LOSSES HP	ELEV. LOSSES HP	NET HP AFTER LOSSES
FUEL	16181					
RATED	4056	32	20	49	-10	3965
NGP	4059	32	20	49	-10	3968
PCD	4011	31	20	45	-10	3924
5	4154	32	20	58	-10	4053
COMP	2437					

	% EFF	
RATED	24.5	RATED NET HP/FUEL GROSS HP
NGP	100.1	NET NGP HP/NET RATED HP
PCD	99.0	NET PCD HP/NET RATED HP
5	102.2	NET T5 HP/NET RATED HP
COMP	61.2	COMPRESSOR HP/AVERAGE NET HP
OVERALL	15.1	COMPRESSOR HP/FUEL HP

#2 Turbine

11/14/90

8:00 AM

-GT - HANOVER COMPRESSOR STATION

SOLAR CENTAUR 3830 NATURAL GAS TURBINE/COMPRESSOR PERFORMANCE

DATE 08:26:11 TIME 11-14-1990

OPERATING CONDITIONS

ASUCTION PRESSURE	615 PSIG	FUEL FLOW	41 MMBTU/H
DISCHARGE PRESSURE	666 PSIG	PCD	124 PSIG
RESSURE RATIO	1.08	T5	1080 DEG F
UCTION TEMPERATURE	74 DEG F	NGP	100 %
DISCHARGE TEMPERATURE	93 DEG F	NPT	87 %
THROUGHPUT	30497 MMBTU/H	FUEL RATIO	0.1 % FUEL/THROUGHPUT
MBIENT TEMPERATURE	35 DEG F		

PERFORMANCE PARAMETERS

	GROSS HP BEFORE LOSSES	INLET LOSSES HP	EXHAUST LOSSES HP	NPT LOSSES HP	ELEV. LOSSES HP	NET HP AFTER LOSSES
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FUEL	16181					
RATED	4040	32	20	48	-10	3949
NGP	4043	32	20	48	-10	3952
CD	4017	31	20	46	-10	3929
5	4061	32	20	50	-10	3969
COMP	2354					

% EFF

RATED	24.4	RATED NET HP/FUEL GROSS HP
NGP	100.1	NET NGP HP/NET RATED HP
CD	99.5	NET PCD HP/NET RATED HP
5	100.5	NET T5 HP/NET RATED HP
COMP	59.6	COMPRESSOR HP/AVERAGE NET HP
VERALL	14.5	COMPRESSOR HP/FUEL HP

#2 Turbine

- 11/14/90

9 AM

_GT - HANOVER COMPRESSOR STATION

SOLAR CENTAUR 3830 NATURAL GAS TURBINE/COMPRESSOR PERFORMANCE

DATE 11:23:54 TIME 11-14-1990

OPERATING CONDITIONS

INLET PRESSURE	612 PSIG	FUEL FLOW	41 MMBTU/H
DISCHARGE PRESSURE	661 PSIG	PCD	123 PSIG
PRESSURE RATIO	1.08	T5	1080 DEG F
INLET TEMPERATURE	74 DEG F	NGP	100 %
DISCHARGE TEMPERATURE	93 DEG F	NPT	87 %
THROUGHPUT	30499 MMBTU/H	FUEL RATIO	0.1 % FUEL/THROUGHPUT
AMBIENT TEMPERATURE	36 DEG F		

PERFORMANCE PARAMETERS

	GROSS HP BEFORE LOSSES	INLET LOSSES HP	EXHAUST LOSSES HP	NPT LOSSES HP	ELEV. LOSSES HP	NET HP AFTER LOSSES
FUEL	16181					
RATED	4031	32	20	48	-10	3941
NGP	4034	32	20	48	-10	3944
CD	3955	31	20	41	-9	3872
5	4045	32	20	49	-10	3954
COMP	2276					

	% EFF	
RATED	24.4	RATED NET HP/FUEL GROSS HP
NGP	100.1	NET NGP HP/NET RATED HP
CD	98.2	NET PCD HP/NET RATED HP
5	100.3	NET T5 HP/NET RATED HP
COMP	58.0	COMPRESSOR HP/AVERAGE NET HP
OVERALL	14.1	COMPRESSOR HP/FUEL HP

#2 Turbine

11/14/90

10 AM

NGT - HANOVER COMPRESSOR STATION
SOLAR CENTAUR 3830 NATURAL GAS TURBINE/COMPRESSOR PERFORMANCE
DATE 11:26:30 TIME 11-14-1990

OPERATING CONDITIONS

ASUCTION PRESSURE	610 PSIG	FUEL FLOW	41 MMBTU/H
DISCHARGE PRESSURE	658 PSIG	PCD	123 PSIG
RESSURE RATIO	1.08	T5	1090 DEG F
UCTION TEMPERATURE	74 DEG F	NGP	100 %
DISCHARGE TEMPERATURE	91 DEG F	NPT	87 %
THROUGHPUT	30486 MMBTU/H	FUEL RATIO	0.1 % FUEL/THROUGHPUT
MBIENT TEMPERATURE	39 DEG F		

PERFORMANCE PARAMETERS

	GROSS HP BEFORE LOSSES	INLET LOSSES HP	EXHAUST LOSSES HP	NPT LOSSES HP	ELEV. LOSSES HP	NET HP AFTER LOSSES
FUEL	16181					
RATED	4006	31	20	47	-10	3917
NGP	4010	31	20	47	-10	3920
CD	3964	31	20	43	-9	3879
5	4056	32	20	51	-10	3962
COMP	2237					
	% EFF					
RATED	24.2	RATED NET HP/FUEL GROSS HP				
NGP	100.1	NET NGP HP/NET RATED HP				
CD	99.0	NET PCD HP/NET RATED HP				
5	101.2	NET T5 HP/NET RATED HP				
COMP	57.1	COMPRESSOR HP/AVERAGE NET HP				
VERALL	13.8	COMPRESSOR HP/FUEL HP				

#2 Turbine

- 11/14/90

11 AM

NGT - HANOVER COMPRESSOR STATION

SOLAR CENTAUR 3830 NATURAL GAS TURBINE/COMPRESSOR PERFORMANCE

ATE 11:29:21 TIME 11-14-1990

OPERATING CONDITIONS

SUCTION PRESSURE	608 PSIG	FUEL FLOW	41 MMBTU/H
DISCHARGE PRESSURE	657 PSIG	PCD	122 PSIG
RESSURE RATIO	1.08	T5	1090 DEG F
SUCTION TEMPERATURE	74 DEG F	NGP	100 %
DISCHARGE TEMPERATURE	93 DEG F	NPT	87 %
THROUGHPUT	30277 MMBTU/H	FUEL RATIO	0.1 % FUEL/THROUGHPUT
MBIENT TEMPERATURE	42 DEG F		

PERFORMANCE PARAMETERS

	GROSS HP BEFORE LOSSES	INLET LOSSES HP	EXHAUST LOSSES HP	NPT LOSSES HP	ELEV. LOSSES HP	NET HP AFTER LOSSES
UEL	16181					
RATED	3981	31	20	46	-9	3893
NGP	3985	31	20	46	-9	3897
CD	3908	31	20	40	-9	3827
5	4008	31	20	48	-10	3917
COMP	2274					

	% EFF	
RATED	24.1	RATED NET HP/FUEL GROSS HP
NGP	100.1	NET NGP HP/NET RATED HP
CD	98.3	NET PCD HP/NET RATED HP
T5	100.6	NET T5 HP/NET RATED HP
COMP	58.6	COMPRESSOR HP/AVERAGE NET HP
VERALL	14.1	COMPRESSOR HP/FUEL HP

#2 Turbine

11/14/90

12:30 PM

GT - HANOVER COMPRESSOR STATION

SOLAR CENTAUR 3830 NATURAL GAS TURBINE/COMPRESSOR PERFORMANCE

DATE 14:28:46 TIME 11-14-1990

OPERATING CONDITIONS

SUCTION PRESSURE	604 PSIG	FUEL FLOW	41 MMBTU/H
DISCHARGE PRESSURE	652 PSIG	PCD	122 PSIG
PRESSURE RATIO	1.08	T5	1100 DEG F
SUCTION TEMPERATURE	72 DEG F	NGP	100 %
DISCHARGE TEMPERATURE	90 DEG F	NPT	87 %
THROUGHPUT	30230 MMBTU/H	FUEL RATIO	0.1 % FUEL/THROUGHPUT
AMBIENT TEMPERATURE	45 DEG F		

PERFORMANCE PARAMETERS

	GROSS HP BEFORE LOSSES	INLET LOSSES HP	EXHAUST LOSSES HP	NPT LOSSES HP	ELEV. LOSSES HP	NET HP AFTER LOSSES
FUEL	16181					
RATED	3957	31	20	45	-9	3870
NGP	3960	31	20	45	-9	3873
PCD	3916	31	20	42	-9	3833
5	4019	31	20	50	-10	3926
COMP	2230					
	% EFF					
RATED	23.9	RATED NET HP/FUEL GROSS HP				
NGP	100.1	NET NGP HP/NET RATED HP				
CD	99.1	NET PCD HP/NET RATED HP				
5	101.5	NET T5 HP/NET RATED HP				
COMP	57.5	COMPRESSOR HP/AVERAGE NET HP				
OVERALL	13.8	COMPRESSOR HP/FUEL HP				

#2 Turbine

11/14/90

1:00 PM

GT - HANOVER COMPRESSOR STATION
SOLAR CENTAUR 3830 NATURAL GAS TURBINE/COMPRESSOR PERFORMANCE
ATE 14:26:26 TIME 11-14-1990

OPERATING CONDITIONS

INLET PRESSURE	602 PSIG	FUEL FLOW	41 MMBTU/H
DISCHARGE PRESSURE	650 PSIG	PCD	122 PSIG
PRESSURE RATIO	1.08	T5	1100 DEG F
INLET TEMPERATURE	74 DEG F	NGP	100 %
DISCHARGE TEMPERATURE	94 DEG F	NPT	87 %
THROUGHPUT	29857 MMBTU/H	FUEL RATIO	0.1 % FUEL/THROUGHPUT
AMBIENT TEMPERATURE	46 DEG F		

PERFORMANCE PARAMETERS

	GROSS HP BEFORE LOSSES	INLET LOSSES HP	EXHAUST LOSSES HP	NPT LOSSES HP	ELEV. LOSSES HP	NET HP AFTER LOSSES
FUEL	16181					
RATED	3948	31	20	45	-9	3862
NGP	3952	31	20	45	-9	3865
CD	3919	31	20	42	-9	3835
_5	4003	31	20	49	-9	3911
COMP	2221					

	% EFF	
RATED	23.9	RATED NET HP/FUEL GROSS HP
NGP	100.1	NET NGP HP/NET RATED HP
CD	99.3	NET PCD HP/NET RATED HP
_5	101.3	NET T5 HP/NET RATED HP
COMP	57.4	COMPRESSOR HP/AVERAGE NET HP
VERALL	13.7	COMPRESSOR HP/FUEL HP

#2 Turbine

11/14/90

2:00 PM

AGT - HANOVER COMPRESSOR STATION
SOLAR CENTAUR 3830 NATURAL GAS TURBINE/COMPRESSOR PERFORMANCE
DATE 14:22:27 TIME 11-14-1990

OPERATING CONDITIONS

SUCTION PRESSURE	602 PSIG	FUEL FLOW	41 MMBTU/H
DISCHARGE PRESSURE	650 PSIG	PCD	121 PSIG
PRESSURE RATIO	1.08	T5	1100 DEG F
SUCTION TEMPERATURE	76 DEG F	NGP	100 %
DISCHARGE TEMPERATURE	96 DEG F	NPT	87 %
THROUGHPUT	29596 MMBTU/H	FUEL RATIO	0.1 % FUEL/THROUGHPUT
AMBIENT TEMPERATURE	47 DEG F		

PERFORMANCE PARAMETERS

	GROSS HP BEFORE LOSSES	INLET LOSSES HP	EXHAUST LOSSES HP	NPT LOSSES HP	ELEV. LOSSES HP	NET HP AFTER LOSSES
FUEL	16181					
RATED	3940	31	20	45	-9	3854
NGP	3944	31	20	45	-9	3857
PCD	3858	31	19	38	-9	3779
T5	3986	31	20	48	-9	3896
COMP	2212					
	% EFF					
RATED	23.8	RATED NET HP/FUEL GROSS HP				
NGP	100.1	NET NGP HP/NET RATED HP				
PCD	98.1	NET PCD HP/NET RATED HP				
T5	101.1	NET T5 HP/NET RATED HP				
COMP	57.5	COMPRESSOR HP/AVERAGE NET HP				
OVERALL	13.7	COMPRESSOR HP/FUEL HP				

APPENDIX E
Calculations

CALCULATIONS

ALL PARAMETERS

1) Actual gas CONCENTRATION

$$\text{CONC.}_{\text{ACTUAL}} = (\text{CONC.}_{\text{STRIP CHART AVERAGE}} - \text{zero cal.}) \frac{\text{Actual gas bottle conc.}}{(\text{Upscale cal.} - \text{zero cal.})}$$

EXAMPLE: TEST #1 UNIT #1 NO_x

$$\text{ppm} = (74.5 - 0.0) \frac{(143)}{(135.1 - 0.0)}$$

$$\text{ppm} = 78.9$$

2) Emission Rate

$$\text{lbs/hr} = \text{ppm} \times \text{DSCFM} \times \text{Molecular weight} \times 15.58 \times 10^{-8}$$

EXAMPLE: TEST #1 UNIT #1 NO_x as NO

$$\text{lbs/hr} = (78.9)(37500)(30)(15.58 \times 10^{-8})$$

$$\text{lbs/hr} = 13.8$$

NO_x ONLY

3 CONCENTRATION CORRECTED TO 15% OXYGEN

$$\text{NO}_x_{15\% \text{ O}_2} = (\text{NO}_x \text{ ppm}) \left(\frac{20.9 - 15.0}{20.9 - \text{O}_2} \right)$$

EXAMPLE TEST #1 UNIT #1

$$= (78.9) \left(\frac{20.9 - 15.0}{20.9 - 17.0} \right)$$

$$= 125.8 \text{ ppm}$$

4. ISO K factor

$$\text{ISO K FACTOR} = \left(\frac{\text{combustor inlet pressure}_{\text{ref}}}{\text{combustor inlet pressure}_{\text{amb}}} \right)^{0.5} \left(e^{19(\text{humidity}_{\text{ambient}} - 0.00633)} \right) \\ \rightarrow \times \left(\frac{288^{\circ}\text{K}}{T_{\text{amb}}^{\circ}\text{K}} \right)^{1.53}$$

EXAMPLE: TEST #1 UNIT #1

$$\text{combustor inlet pressure}_{\text{amb}} = 122 \text{ psi} = 248.4 \text{ in Hg}$$

$$\text{combustor inlet pressure}_{\text{ref}} = 248.4 \text{ in Hg} \left(\frac{30.05 \text{ in Hg}}{29.92 \text{ in Hg}} \right) = 249.5$$

$$\text{humidity}_{\text{ambient}} = \frac{\% \text{ Relative humidity}}{100} \left[\frac{\text{saturation vapor pressure}^*}{1.61 (\text{combustor inlet pressure}_{\text{amb}} - \text{saturation vapor press})} \right] \\ = \frac{40}{100} \left[\frac{0.274}{1.61 (248.4 - 0.274)} \right] \\ = 0.000274$$

$$\text{ISO K FACTOR} = \left(\frac{249.5}{248.4} \right)^{0.5} \left(e^{19(0.000274 - 0.00633)} \right) \left(\frac{288^{\circ}\text{K}}{277.4^{\circ}\text{K}} \right)^{1.53} \\ = 0.946$$

5. NO_x CONCENTRATION CORRECTED TO 15% OXYGEN AT ISO CONDITIONS

$$\text{NO}_x @ 15\% \text{ O}_2 @ \text{ISO} = (\text{NO}_x @ 15\% \text{ O}_2) (\text{ISO K FACTOR})$$

EXAMPLE TEST #1 UNIT #1

$$= (125.8) (0.946) \\ = 119.0 \text{ ppm}$$

* see table on next page

APPENDIX F
CEM Data Summary

CEM DATA

AVERAGE PPM BEFORE CALIBRATION BIAS ADJUSTMENT
UNIT # 1
TEST # 1

NOX = 74.5 CO = 6.7 THC = 0.3 O₂ = 17.2

TEST # 2

NOX = 51.6 CO = 7.6 THC = 2.5 O₂ = 18.1

TEST # 3

NOX = 88.0 CO = 7.8 THC = 0.2 O₂ = 17.2

UNIT # 2

TEST # 1

NOX = 63.3 CO = 8.2 THC = 0.3 O₂ = 17.6

TEST # 2

NOX = 72.3 CO = 6.9 THC = 0.1 O₂ = 17.1

TEST # 3

NOX = 71.6 CO = 9.2 THC = 0.2 O₂ = 17.1

