

Commonwealth of Pennsylvania
Environmental Resources
October 10, 1991

Subject: Source Test Review

To: Data File
Philadelphia Electric Company
Croyden Generating Station
Croyden, Montgomery County

From: William Schneider *WS*
Air Pollution Control Engineer
Division of Technical Services and Monitoring
Bureau of Air Quality Control

Through: Chief, Source Testing and Monitoring Section *JM*

Philadelphia Electric Company (PECO) operates Combustion Turbine Units 11, 21, and 22 at its Croyden generating facility. Gilbert/Commonwealth, Inc. conducted three NO_x Method 7D tests and three CO Method 10B tests simultaneously at each unit on July 16-18, 1991. Sampling was conducted at the transition between the diffuser and regenerator at each turbine unit. This location was necessary because leakage of the generator would likely reduce the NO_x and CO concentrations if sampling was performed in the exhaust stack. An attempt was made to conduct sampling at near maximum load for the combustion turbine. A pretest protocol was approved by the Department.

All tests are acceptable to the Department.

NO_x Emissions (lbs/mmBtu)

Unit	Run No. 1	Run No. 2	Run No. 3
11	1.12	1.21	1.11
21	1.12	1.08	1.09
22	0.54	0.54	0.56

CO Emissions (lbs/mmBtu)

Unit	Run No. 1	Run No. 2	Run No. 3
11	0.00372	0.00418	0.00507
21	0.00280	0.00284	0.00308
22	0.00226	0.00270	0.00376

Unit 11 Operating Conditions

Run No. 1	Run No. 2	Run No. 3
Flue Gas Flow (DSCFM) 323,186	334,679	336,084
Turbine Load (MW) 29	29	27

Unit 21 Operating Conditions

Run No. 1	Run No. 2	Run No. 3
Flue Gas Flow (DSCFM) 373,508	367,106	388,583
Turbine Load (MW) 45	43	42

Unit 22 Operating Conditions

Run No. 1	Run No. 2	Run No. 3
Flue Gas Flow (DSCFM) 382,376	367,946	366,803
Turbine Load (MW) 47	47	45

cc: A.P. File
Edward Brown, Southeast Regional Office
Krishnan Ramamurthy, A&C
EPA/RSL
Reading File - Source Testing

WS:lk

SOURCE SAMPLING REPORT FOR MEASUREMENT
OF NO_x AND CO EMISSIONS

COMBUSTION TURBINE UNITS 11, 21, AND 22

PHILADELPHIA ELECTRIC COMPANY
CROYDON GENERATING STATION
CROYDON, PA

G/C, INC., REPORT R-04-6314-000
AUGUST, 1991

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CROYDON GENERATING STATION
CROYDON, PA

G/C, INC., REPORT R-04-6314-000
AUGUST, 1991

PREPARED BY

GILBERT/COMMONWEALTH, INC.
P.O. BOX 1498
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ERIC ROLAND
ENVIRONMENTAL SPECIALIST
TESTING SERVICES GROUP

FOREWORD

The source sampling program as defined by this report was confined to the measurement of NO_x and CO emissions and pertinent exhaust gas characteristics at referenced operating conditions for the combustion turbine units No. 11, 21, and 22 at your Croydon Generating Station.

The sampling program was performed according to procedures specified by the Federal Environmental Protection Agency and by the Pennsylvania Department of Environmental Resources.

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SECTION I
SUMMARY OF TEST RESULTS

SECTION I - SUMMARY OF TEST RESULTS

Unit 11 running at an average load of 28.3 MW had average flue gas characteristics of 16.43% O₂, 2.95% CO₂, and 3.4% moisture. The NO_x emissions were an average of 1.146 LBS/MMBTU. CO emissions were an average of 0.00432 LBS/MMBTU.

Unit 21 running at an average load of 43 MW had average flue gas characteristics of 16.49% O₂, 2.74% CO₂, and 3.0% moisture. The NO_x emissions were an average of 1.099 LBS/MMBTU. CO emissions were an average of 0.00291 LBS/MMBTU.

Unit 22 running at an average load of 46.3 MW had average flue gas characteristics of 15.19% O₂, 3.73% CO₂, and 4.1% moisture. The NO_x emissions were an average of 0.547 LBS/MMBTU. CO emissions were an average of 0.00291 LBS/MMBTU.

These results are detailed in Tables 1-4.

O₂ traverses completed on each unit showed no signs of stratification.

TABLE 1
 SUMMARY OF TEST RESULTS
 PHILADELPHIA ELECTRIC COMPANY
 CROYDON STATION
 G/C, INC. REPORT R-04-6314-000

DATE	7/16/91	7/17/91	7/18/91
UNIT	11	21	22
RUN NO.	1-3	1-3	1-3
TIME	1014-1355	0844-1212	0934-1247
LOAD (MW)	28.3	43	46.3
<u>FLUE GAS CHARACTERISTICS</u>			
DSCFM	331,316	376,399	372,375
O ₂ , %	16.43	16.49	15.19
CO ₂ , %	2.95	2.74	3.73
MOISTURE, %	3.4	3.0	4.1
<u>NO_x EMISSIONS</u>			
PPM	210.7	202.6	128.5
LBS/HR	500.02	545.77	342.77
LBS/MMMBTU	1.146	1.099	0.547
MMBTU/HR	436.0	496.7	630.7
<u>SO₂ EMISSIONS</u>			
PPM	1.33	0.90	1.17
LBS/HR	1.88	1.44	1.83
LBS/MMMBTU	0.00432	0.00291	0.00291

TABLE 2
SUMMARY OF TEST RESULTS
PHILADELPHIA ELECTRIC COMPANY
CROYDON STATION
G/C, INC. REPORT R-04-6314-000

DATE	7/16/91		
UNIT	11		
RUN NO.	1	2	3
TIME	1014-1114	1137-1237	1255-1355
LOAD (MW)	29	29	27
<u>FLUE GAS CHARACTERISTICS</u>			
DSCFM	323,186	334,679	336,084
O ₂ , %	16.25	16.40	16.63
CO ₂ , %	3.03	3.03	2.80
MOISTURE, %	3.4	3.4	3.4
<u>NO_x EMISSIONS</u>			
PPM	214.7	223.3	194.2
LBS/HR	497.20	535.34	467.51
LBS/MMBTU	1.12	1.21	1.11
MMBTU/HR	443.0	442.0	423.0
<u>SO₂ EMISSIONS</u>			
PPM	1.20	1.30	1.50
LBS/HR	1.65	1.85	2.15
LBS/MMBTU	0.00372	0.00418	0.00507

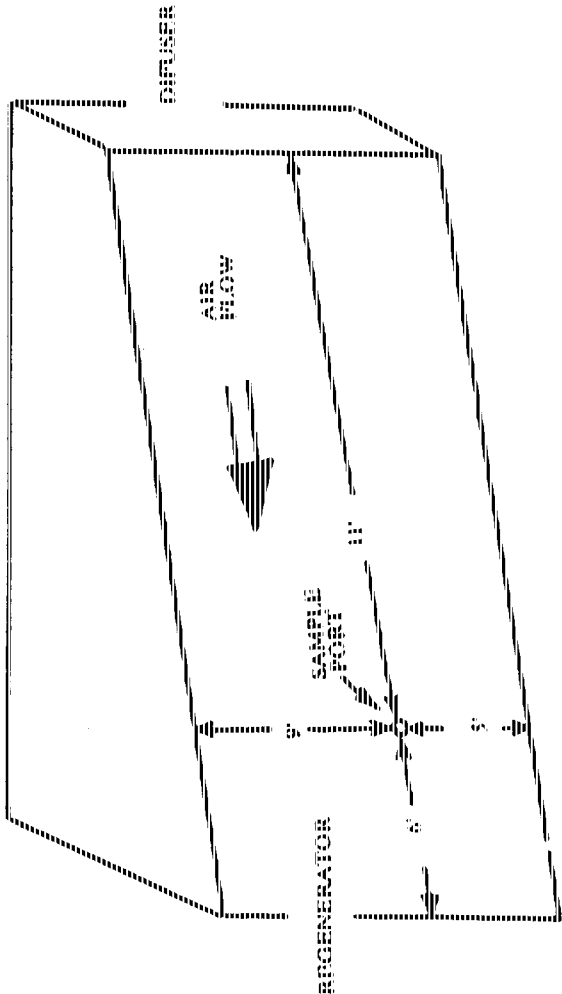
TABLE 3

SUMMARY OF TEST RESULTS
 PHILADELPHIA ELECTRIC COMPANY
 CROYDON STATION
 G/C, INC. REPORT R-04-6314-000

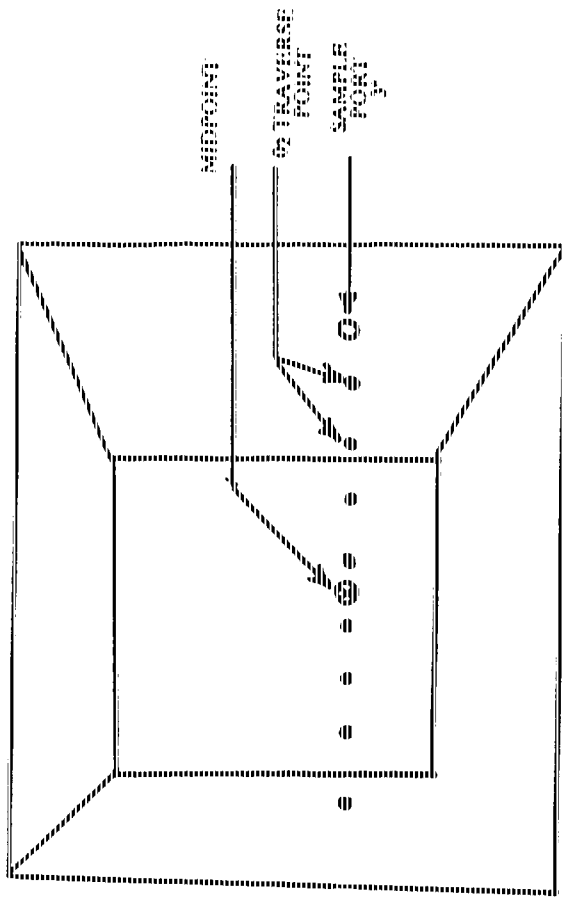
DATE	7/17/91		
UNIT	21		
RUN NO.	1	2	3
TIME	0844-0944	0958-1058	1112-1212
LOAD (MW)	45	43	42
<u>FLUE GAS CHARACTERISTICS</u>			
DSCFM	373,508	367,106	388,583
O ₂ %	16.33	16.40	16.73
CO ₂ %	2.85	2.73	2.65
MOISTURE, %	3.0	3.0	3.0
<u>NO_x EMISSIONS</u>			
PPM	214.3	203.9	189.5
LBS/HR	573.54	536.15	527.63
LBS/MMBTU	1.12	1.08	1.09
MMBTU/HR	510.0	495.0	485.0
<u>CO EMISSIONS</u>			
PPM	0.90	0.90	0.90
LBS/HR	1.43	1.41	1.49
LBS/MMBTU	0.00280	0.00284	0.00308

TABLE 4
 SUMMARY OF TEST RESULTS
 PHILADELPHIA ELECTRIC COMPANY
 CROYDON STATION
 G/C, INC. REPORT R-04-6314-000

DATE	7/18/91		
UNIT	22		
RUN NO.	1	2	3
TIME	0934-1034	1041-1141	1147-1247
LOAD (MW)	47	47	45
<u>ELUE GAS CHARACTERISTICS</u>			
DSCFM	382,376	367,946	366,803
O ₂ %	15.23	15.10	15.25
CO ₂ %	3.80	3.85	3.53
MOISTURE, %	4.1	4.1	4.1
<u>NO_x EMISSIONS</u>			
PPM	125.8	129.1	130.7
LBS/HR	344.71	340.25	343.34
LBS/MMBTU	0.54	0.54	0.56
MMBTU/HR	642.0	632.0	618.0
<u>CO EMISSIONS</u>			
PPM	0.90	1.10	1.50
LBS/HR	1.45	1.71	2.33
LBS/MMBTU	0.00226	0.00270	0.00376



TRANSITION
PLAN VIEW



TRANSITION
CROSS SECTION VIEW
LOOKING INTO DIFFUSER

POINT NO.	ϕ TRAVERSE	DISTANCE FROM PORT
1		15'
2		33'
3		51'
4		69'
5		87'
6		105'
7		123'
8		141'

FIGURE 1 - PHILADELPHIA ELECTRIC COMPANY
CROYDON GENERATING STATION
COMBUSTION TURBINE UNITS 11, 21, AND 22
SAMPLING LOCATION

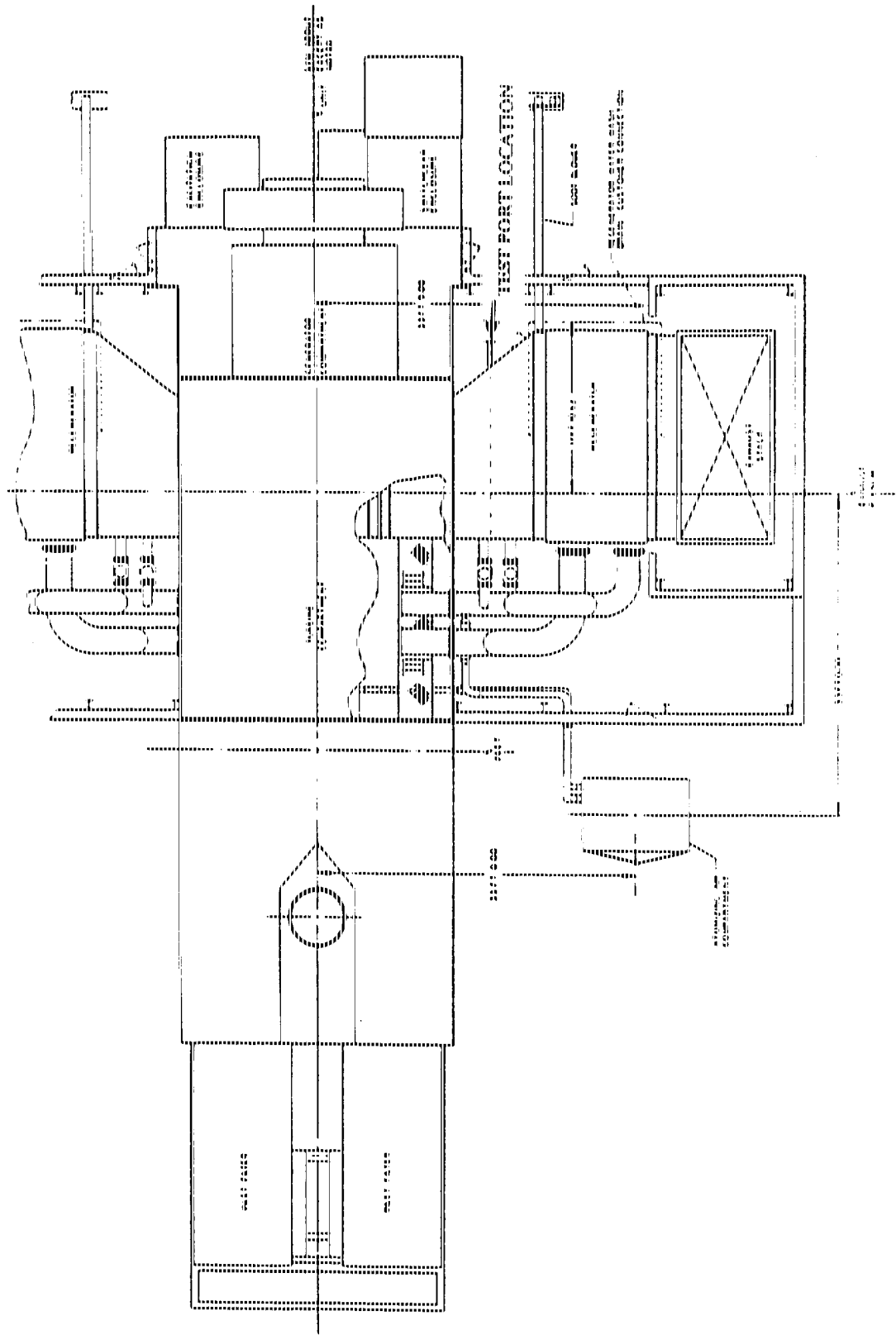


FIGURE 2 - PHILADELPHIA ELECTRIC COMPANY
 CROYDON GENERATING STATION
 COMBUSTION TURBINE UNITS 11, 21, AND 22

SECTION II
ANALYSES

SECTION II - ANALYSIS

1. Introduction

The data presented in this report represents the results of source sampling exhaust emissions located in the transition between the diffuser and regenerator for Combustion Turbine Units 11, 21, and 22 (Figure 1). Sampling was performed while the units were maintained at normal operating conditions.

Specific requirements of this source sampling program are as follows:

- a. Identification of NO_x and CO emissions from the transition between the diffuser and regenerator for compliance with existing pollution control regulations.
- b. O_2 traverse to determine the extent of O_2 stratification across the duct.
- c. Percent moisture of the exhaust gas.
- d. Orsat analysis of exhaust gas conditions.
- e. Fuel analysis of fuel burned during the test period.
- f. Combustion calculations to determine flue gas flow.

Field work for the sampling program was completed on July 16, 17, and 18, 1991. The sampling program was completed by the Gilbert field test crew with the assistance of PECO personnel.

2. Sampling Program Procedures

To satisfy the objectives for this project, the sampling program was set up on the basis of running one O_2 traverse to determine if any O_2 stratifications existed, followed by three (3) NO_x tests (Method 7D) and three (3) CO tests (Method 10B) simultaneously. A moisture train was then run to determine percent moisture in the exhaust gas. Each unit (11, 21, and 22) was tested independently on separate days. All procedures for the determination of molecular weight, moisture content, NO_x , CO, O_2 , and CO_2 concentrations of the exhaust gas were made according to standard test methods as referenced in Appendix 2.

3. Operating Conditions

In the execution of this sampling program an attempt was made to achieve near maximum load for the Combustion Turbine. Details of the operating parameters can be found in the operating data included in Appendix 3.

4. Results

Test data developed by each test run are reproduced in the Appendices included with this report. Information on basic gas characteristics developed by each test run is contained in the printout of the computer program included as Appendix 7.

A summary of pertinent test results and essential information to evaluate test results developed for each test run is included with this report as Tables 1 thru 4.

5. Discussion

Sampling Conditions

All field sampling work was completed at the transition between the diffuser and regenerator and subject to prevailing weather conditions; however, there were no interruptions in the operation of individual test trains due to equipment or weather problems.

During the completion of this test program, the Units were maintained near the normal load condition.

NO_x emissions (ppm) measured by the analyzer were generally steady during the 1 hour test runs and consistent for all three tests.

NO_x emissions in lbs/hour are documented in Tables 1 thru 4.

NO_x emissions in lbs/MMBtu of heat input are documented in Tables 1 thru 4. NO_x lbs/MMBtu were calculated using both CO₂ and O₂ based "F" Factors from the Orsat analysis of the integrated bag samples. The resulting close agreement between the lbs/MMBtu values calculated using the two different "F" Factors indicates that the bag samples and Orsat analysis of the samples were representative of theoretically correct CO₂/O₂ relationships.

CO emissions in PPM and LBS/HR are documented in Tables 1 thru 4.

APPENDIX 1
PROJECT PARTICIPANTS

APPENDIX 1

PROJECT PARTICIPANTS

The following members of Gilbert/Commonwealth staff participated in the planning and execution of this project and preparation of this report.

Field Sampling Crew:

George Albright
Gary Helm
Eric Roland

Project Coordinator
Engineering Technician
Environmental Specialist

Laboratory Participants:

Vaughn O'Neill
Josie King

Chemist
Chemist

All field tests were completed with the assistance of technical personnel from Philadelphia Electric Company.

APPENDIX 2
TESTING AND ANALYTICAL PROCEDURES

- 2.1 NO_x TESTING PROCEDURES
- 2.2 CO TESTING PROCEDURES
- 2.3 O₂ TESTING PROCEDURES

APPENDIX 2

TESTING AND ANALYTICAL PROCEDURES

2.1 NO_x TESTING PROCEDURES

NO_x emissions were sampled according to EPA Method 7D as it appears in 40 CFR, Part 60, Appendix A. Exhaust gas was withdrawn from the sampling point at a rate of approximately 0.4-0.5 liters per minute and passed through three NO_x impingers containing Potassium Permanganate absorbing solution. Each sample run was one-hour in duration. A single moisture run was performed to determine percent moisture in the exhaust gas. Ion chromatography was used to determine micro grams of NO₂ in the sample. The calculations used to determine ppm and lbs/MMBtu of NO_x are shown in Appendix 9.

APPENDIX 2

TESTING AND ANALYTICAL PROCEDURES

2.2 CO TESTING PROCEDURES

CO emissions were sampled in accordance with EPA Method 10B as it appears in 40 CFR, Part 60, Appendix A. Exhaust gas was withdrawn from the sampling point at a rate of approximately 0.3 liters/minute and passed through three impingers containing Potassium Permanganate solution prior to being collected in a Tedlar bag. Each sample run was one-hour in length. CO concentration in the sample bags was determined by gas chromatography. The calculations used to determine ppm (CO) are shown in Appendix 9.

APPENDIX 2

TESTING AND ANALYTICAL PROCEDURES

2.3 O₂ TESTING PROCEDURES

O₂ emissions were sampled according to EPA Method 3 as it appears in 40 CFR, Part 60, Appendix A. The single point, integrated sampling form of Method 3 was used to collect approximately 30 liters of exhaust gas in a Tedlar bag for each one-hour test run. A series of Orsat analyses were performed on the bag sample after the collection period. The average CO₂ and O₂ values of the integrated sample were considered to represent the one-hour average CO₂ and O₂ values. These values are expressed as a dry basis percentage.

A series of single point grab samples were also analyzed during the test period.

APPENDIX 3
UNIT OPERATING DATA

- 3.1 OPERATING DATA - UNIT 11
- 3.2 OPERATING DATA - UNIT 21
- 3.3 OPERATING DATA - UNIT 22

APPENDIX 3
UNIT OPERATING DATA

3.1 OPERATING DATA - UNIT 11

Operating Data - Unit 11

CROYDON STATION
CONTROL ROOM
DAILY OPERATING READINGS

DATE: 2-16-91

INSTRUCTIONS:

1. Readings shall be recorded each day the unit is operated.
2. Report all abnormalities to supervision immediately.
3. Submit readings to Shift Supervisor for review.
4. After review Shift Supervisor shall forward readings to Engineer, Supervisory (R.E.) or his designated representative.

UNIT NO.	11	12	21	22	31	32	41	42
LOAD (MW)	35							
AMBIENT TEMP	74							
EXHAUST TEMP. (A) (900-1090)	1020							
EXHAUST TEMP. (B) (900-1080)	1046							
COMP. DISCH. TEMP (# 600°F)	535							
COMB. MONITOR TEMP SPREAD (# 500°F)	107							
IGV POSITION (deg) (82°)	79							
# BRG. AREA TEMP.	64.9 8-30A							

By: _____

Reviewed By: _____
Sh. Supervisor

Reviewed By: _____
Engr. Supv./STA

M-25249 10/66

CROYDON STATION
CONTROL ROOM
DAILY OPERATING READINGS

DATE: 7-16-97

INSTRUCTIONS:

- 1. Readings shall be recorded each day the unit is operated.
- 2. Report all abnormalities to supervision immediately.
- 3. Submit readings to Shift Supervisor for review.
- 4. After review Shift Supervisor shall forward readings to Engineer, Supervisory (P.E.) or his designated representative.

*Rec'd
7-16-97*

UNIT NO.	11	12	21	22	31	32	41	42
OAD (MW)	<u>29</u>	_____	_____	_____	_____	_____	_____	_____
AMBIENT TEMP	<u>82</u>	_____	_____	_____	_____	_____	_____	_____
EXHAUST TEMP (A) (900-1090)	<u>960</u>	_____	_____	_____	_____	_____	_____	_____
EXHAUST TEMP (B) (900-1080)	<u>960</u>	_____	_____	_____	_____	_____	_____	_____
COMP DISCH. TEMP (2600°F)	<u>550</u>	_____	_____	_____	_____	_____	_____	_____
COMB. MONITOR TEMP SPREAD (250°F)	<u>103</u>	_____	_____	_____	_____	_____	_____	_____
GV POSITION (deg) (32°)	<u>79</u>	_____	_____	_____	_____	_____	_____	_____
BERG. AREA TEMP.	<u>68.1</u>	_____	_____	_____	_____	_____	_____	_____

10 00 14

By: _____

Reviewed By: _____
Sh. Supervisor

Reviewed By: _____
Engr. Supv./STA

CROYDON STATION
CONTROL ROOM
DAILY OPERATING READINGS

DATE: 7-16-91

INSTRUCTIONS:

1. Readings shall be recorded each day the unit is operated.
2. Report all abnormalities to supervision immediately.
3. Submit readings to Shift Supervisor for review.
4. After review Shift Supervisor shall forward readings to Engineer, Supervisory (R.E.) or his designated representative.

UNIT NO.	<u>11</u>	<u>12</u>	<u>21</u>	<u>22</u>	<u>31</u>	<u>32</u>	<u>41</u>	<u>42</u>
LOAD (MW)	<u>29</u>							
AMBIENT TEMP.	<u>86</u>							
EXHAUST TEMP. (A) (900-1090)	<u>265</u>							
EXHAUST TEMP. (B) (900-1080)	<u>260</u>							
COMP. DISCH. TEMP. (2" 600°F)	<u>575</u>							
COMB. MONITOR TEMP. SPREAD (2" 500°F)	<u>103</u>							
IGV POSITION (deg) (82°)	<u>79</u>							
WBRG. AREA TEMP.	<u>682</u>							

RWC by

11 00 A

By:

Reviewed By:
Sh. Supervisor

Reviewed By:
Engr. Supv./STA

CROYDON STATION
CONTROL ROOM
DAILY OPERATING READINGS

DATE: 2-16-87

INSTRUCTIONS:

1. Readings shall be recorded each day the unit is operated.
2. Report all abnormalities to supervision immediately.
3. Submit readings to Shift Supervisor for review.
4. After review Shift Supervisor shall forward readings to Engineer, Supervisory (R.E.) or his designated representative.

UNIT NO.	^{1200.00} 11	12	21	22	31	32	41	42
LOAD (MW)	27							
AMBIENT TEMP.	94							
EXHAUST TEMP. (A) (900-1090)	940							
EXHAUST TEMP. (B) (900-1080)	920							
COMB. DISCH. TEMP. (3" 600°F)	560							
COMB. MONITOR TEMP. SPREAD (2" 600°F)	51							
IGV POSITION (deg) (82°)	79							
ABRG. AREA TEMP.	677							

1-20/87

By:

Reviewed By:
Sh. Supervisor

Reviewed By:
Eng. Supv./STA

APPENDIX 3
UNIT OPERATING DATA

3.2 OPERATING DATA - UNIT 21

Operating Data - Unit 21

249 10/86

CROYDON STATION
CONTROL ROOM
DAILY OPERATING READINGS

DATE: 7-17-91

INSTRUCTIONS:

- Readings shall be recorded each day the unit is operated.
- Report all abnormalities to supervision immediately.
- Submit readings to Shift Supervisor for review.
- After review Shift Supervisor shall forward readings to Engineer, Supervisory (P.E.) or his designated representative.

	11	12	21	22	31	32	41	42
INCH								
COND (MW)			46					
COND. INLET TEMP			74					
EXHAUST TEMP (A) (1000)			282					
EXHAUST TEMP (B) (800-1080)			1000					
COND. (P) DISCH. TEMP. (200F)			62.2					
COND. MONITOR TEMP SPREAD (200F)			47					
COND. POSITION (deg) (82°)			81					
COND. AREA TEMP			611					

By: _____

Reviewed By: _____
Sh. Supervisor

Reviewed By: _____
Eng. Supv./STA

25249 10/86

CROYDON STATION
CONTROL ROOM
DAILY OPERATING READINGS

DATE: 7-17-91

INSTRUCTIONS:

- Readings shall be recorded each day the unit is operated.
- Report all abnormalities to supervision immediately.
- Submit readings to Shift Supervisor for review.
- After review Shift Supervisor shall forward readings to Engineer, Supervisory (R.E.) or his designated representative.

9:25 AM
DROPPED
LOADS

UNIT NO.	11	12	21	41	31	32	41	42
LOAD (MW)			45	43				
Ambient Temp			76	79				
EXHAUST TEMP. (A) (900-1080)			970	960				
EXHAUST TEMP. (B) (900-1080)			1000	990				
TEMP. DISCH. TEMP. (600PF)			625	628				
COMB. MONITOR TEMP. SPREAD (25-50PF)			47	43				
VALVE POSITION (deg) (82°)			80	80				
REG. AREA TEMP.			676	688				

TEST

By: _____

Reviewed By: _____
Sh. Supervisor

Reviewed By: _____
Engr. Supv./SITA

25249 10/86

CROYDON STATION
CONTROL ROOM
DAILY OPERATING READINGS

DATE: 7-17-91

INSTRUCTIONS:

- 1. Readings shall be recorded each day the unit is operated.
- 2. Report all abnormalities to supervision immediately.
- 3. Submit readings to Shift Supervisor for review.
- 4. After review, Shift Supervisor shall forward readings to Engineer, Supervisory (P.L.E.) or his designated representative.

UNIT NO.	11	12	21	22	31	32	41	42
DAD (MW)			43					
AMBIENT TEMP.			80					
EXHAUST TEMP. (A) (00-1080)			950					
EXHAUST TEMP. (B) (00-1080)			980					
COMP. DISCH. TEMP. (2-600FF)			602					
COMP. MONITOR TEMP SPREAD (2-50FF)			30					
IGV POSITION (deg) 320			82					
REG. AREA TEMP.			683					

TEST 2

By: _____

Reviewed By: _____
Sh. Supervisor

Reviewed By: _____
Eng. Supervisor

7 05249 10/86

CROYDON STATION
CONTROL ROOM
DAILY OPERATING READINGS

DATE: 7-17-91

INSTRUCTIONS:

- 1. Readings shall be recorded each day the unit is operated.
- 2. Report all abnormalities to supervision immediately.
- 3. Submit readings to Shift Supervisor for review.
- 4. After review Shift Supervisor shall forward readings to Engineer, Supervisory (F.L.E.) or his designated representative.

UNIT NO.	11	12	21	22	31	32	41	42
LOAD (MW)			472					
BIENT TEMP			94					
EXHAUST TEMP. (A) (700-1090)			95.5					
EXHAUST TEMP. (B) (900-1090)			93.0					
IMP. DISCH. TEMP (600°F)			61.2					
COMB. MONITOR TEMP SPREAD (50°F)			4.5					
VALVE POSITION (deg) (82°)			82					
IRG. AREA TEMP.			65.7					

TEST 3

By: _____

Reviewed By: _____
Sh. Supervisor

Reviewed By: _____
Eng. Supervisor

APPENDIX 3
UNIT OPERATING DATA

3.3 OPERATING DATA - UNIT 22

Operating Data - Unit 22

CROYDON STATION
CONTROL ROOM
DAILY OPERATING READINGS

DATE: 7-18-91

INSTRUCTIONS:

1. Readings shall be recorded each day the unit is operated.
2. Report all abnormalities to supervision immediately.
3. Submit readings to Shift Supervisor for review.
4. After review Shift Supervisor shall forward readings to Engineer, Supervisory (R.E.) or his designated representative.

UNIT NO.	<u>11</u>	<u>12</u>	<u>21</u>	<u>22</u>	<u>31</u>	<u>32</u>	<u>41</u>	<u>42</u>
LOAD (MW)				<u>19</u>				
AMBIENT TEMP				<u>79</u>				
EXHAUST TEMP (A) (900-1090)				<u>1003</u>				
EXHAUST TEMP (B) (900-1080)				<u>922</u>				
COMP. DISCH. TEMP. (2500°F)				<u>600</u>				
COMB. MONITOR TEMP SPREAD (2500°F)				<u>60</u>				
IGV POSITION (deg) (82)				<u>81</u>				
FRIG AREA TEMP				<u>60</u>				

By:

Reviewed By:
Sh. Supervisor

Reviewed By:
Engr. Supervisor

CROYDON STATION
CONTROL ROOM
DAILY OPERATING READINGS

DATE: 7-18-91

INSTRUCTIONS:

1. Readings shall be recorded each day the unit is operated.
2. Report all abnormalities to supervision immediately.
3. Submit readings to Shift Supervisor for review.
4. After review Shift Supervisor shall forward readings to Engineer, Supervisory (P.E.) or his designated representative.

UNIT NO.	11	12	21	22	31	32	41	42
LOAD (MW)				47				
AMBIENT TEMP.				81				
EXHAUST TEMP. (A) (900-1090)				1200				
EXHAUST TEMP. (B) (900-1090)				93.3				
COMP. DISCH. TEMP. (# 500°F)				620				
COMB. MONITOR TEMP. SPREAD (2-50°F)				3.9				
GV POSITION (deg) (82°)				81				
ABRG. AREA TEMP.				551				

TEST-1

By: _____

Reviewed By: _____
Sh. Supervisor

Reviewed By: _____
Engr. Supv./STA

14-25249 10/86

CROYDON STATION
CONTROL ROOM
DAILY OPERATING READINGS

DATE: 7-18-91

INSTRUCTIONS:

1. Readings shall be recorded each day the unit is operated.
2. Report all abnormalities to supervision immediately.
3. Submit readings to Shift Supervisor for review.
4. After review Shift Supervisor shall forward readings to Engineer, Supervisory (R.E.) or his designated representative.

UNIT NO.	11	12	21	22	31	32	41	42
LOAD (MW)				47				
AMBIENT TEMP.				85				
EXHAUST TEMP. (A) (900-1090)				1000				
EXHAUST TEMP. (B) (900-1080)				980				
COMP. DISCH. TEMP. (600°F)				630				
COMB. MONITOR TEMP. SPREAD (250°F)				43				
FLY POSITION (deg) (82°)				81				
BRIG. AREA TEMP.				62.7				

By: _____

Reviewed By: _____
Sh. Supervisor

Reviewed By: _____
Engr. Supv./STA

TEST-2

CROYDON STATION
CONTROL ROOM
DAILY OPERATING READINGS

DATE: 7-18-91

INSTRUCTIONS:

1. Readings shall be recorded each day the unit is operated.
2. Report all abnormalities to supervision immediately.
3. Submit readings to Shift Supervisor for review.
4. After review Shift Supervisor shall forward readings to Engineer, Supervisory (R.E.) or his designated representative.

UNIT NO.	11	12	21	22	31	32	41	42
LOAD (MW)				45				
WBIENT TEMP.				89				
EXHAUST TEMP. (A) (900-1090)				980				
EXHAUST TEMP. (B) (900-1090)				970				
COMP. DISCH. TEMP. (600°F)				615				
COMB. MONITOR TEMP. SPREAD (650°F)				38				
SV POSITION (deg) (82°)				81				
REG. AREA TEMP.				59.5				

By: _____

Reviewed By: _____
Sh. Supervisor

Reviewed By: _____
Engr. Supv./STA

TEST - 3

APPENDIX 4

RAW DATA

- 4.1 NO_x, MOISTURE, O₂ TRAVERSE - UNIT 11
- 4.2 NO_x, MOISTURE, O₂ TRAVERSE - UNIT 21
- 4.3 NO_x, MOISTURE, O₂ TRAVERSE - UNIT 22

APPENDIX 4

RAW DATA

4.1 NO_x, MOISTURE, O₂ TRAVERSE - UNIT 11

GILBERT ASSOCIATES, INC.
ENGINEERS AND CONSULTANTS
READING, PA.

CLIENT PECO

NOX-11-2

P. O. PAGE

OF

Unit 11

7/16/79

DATE

DATE

TEMP

START	TIME	METER	IN	OUT	ORIENT	VAC.
	0	390.330	79	81	0	
1	5	390.393	86	85	0	
2	10	390.4	87	86	0	
3	15	390.493	88	87	0	
4	20	390.548	89	88	0	
5	25	390.610	91	89	0	
6	30	390.5	92	90	0	
7	35	390.721	93	91	0	
8	40		94	92	0	
9	45	390.840	95	93	0	
10	50	390.900	94	93	0	
11	55	390.952	94	93	0	
END	60	391.018			0	

TEMP	A	START	FINISH	NET	D	START	FINISH	NET
"	B				E			
"	C							

GEL	START	FINISH	NET

BAROMETER 30.19

STACK TEMP 971

CONTROL BOX NO. 1385

STATIC $\gamma = 1.03$
+ 13.8" H₂O

CO ₂	NET CO ₂
3.0	19.0
3.3	19.8
2.9	19.0
2.9	19.3

Time
1012
778360
781576

GILBERT ASSOCIATES, INC.
ENGINEERS AND CONSULTANTS
READING, PA.

CLIENT

PECO

Cheydon Station

N.O.

PAGE

OF

UNIT 11

NOX-11-2

7/16/99

DATE

DATE

	TIME	METERS	TEMP		DELTA	VAC.
			IN	OUT		
START	137	0	391.042	95	93	0
1		5	391.110	95	94	0
2		10	391.149	95	95	0
3		15	391.202	95	94	0
4		20	391.253	98	96	0
5		25		98	96	0
6		30	391.303	98	96	0
7		35	391.409	98	97	0
8		40	391.456	99	97	0
9		45	391.510	99	99	0
10		50	391.562	99	99	0
11		55	391.628	99	99	0
END		60	391.682			

	START	FINISH	NET	STOP	FINISH	NET
TEMP A				D		
" B				E		
" C						

	START	FINISH	NET
GEL			

Time
1138

oil (gallons)
782969
786199

BAROMETER 30.18

1238

STACK TEMP. 978

ORSAT

CO ₂	O ₂	NET O ₂
2.8	19.3	16.5
2.9	19.3	16.4
3.1	19.5	16.4
2.2	19.1	16.3

CONTROL BOX NO. 1285

$\gamma = 1.03$

Stack + 13.9" H₂O

GILBERT ASSOCIATES, INC.
ENGINEERS AND CONSULTANTS
READING, PA.

CLIENT

PECO

Clyden

Station

NO.

PAGE

OF

NO. - 11-3

DATE

7/15/91

DATE

TEMP

	TIME	METER	IN	OUT	DIFFER	VAC.
START	1255	0	391.714	99	98	0
1	5	391.772	99	98	0	
2	10	391.843	100	99	0	
3	15	391.900	101	100	0	
4	20	391.965	101	100	0	
5	25	392.028	101	100	0	
6	30	392.096	102	101	0	
7	35	392.151	102	101	0	
8	40	392.215	102	101	0	
9	45	392.275	101	100	0	
10	50	392.339	101	100	0	
11	55	392.405	101	100	0	
END	60	392.462				

	START	FINISH	NET	START	FINISH	NET
IMP A				0		
" B				0		
" C						

	START	FINISH	NET
GEL.			

oil (Gallons)

787.88

290.260

BAROMETER 30.11

1257

1357

STACK TEMP. 950

ORSAT

CO ₂	O ₂	NET O ₂
7.9	19.5	11.6
2.7	19.0	16.3
2.8	19.6	16.8
2.8	19.6	16.8

CONTROL BOX NO. 1315

V = 1.03

Station + 13.9

Date: 7-16-91

Moisture Determination

Run #: UNIT 11

Point	Clock Actual	Time Run	Dry Gas Meter ft.	Orifice Pressure in. HO	Dry Gas Temp (F) Inlet	Dry Gas Temp (F) Outlet
1		0.0	392.539	1.95"	103	102
		3.5	-	1.95"	103	103
2		7.0	398.1	1.95"	103	103
		10.5	-	1.95"	103	103
3		14.0	407.3	1.95"	103	103
		17.5	-	1.95"	103	103
		21.0	407.513			

Y = Meter Factor = 1.03

Barometric Pressure: 30.18 in. Hg , BP
 Net Volume: 15.225 Cubic ft. , VM
 Avg. Orifice: 1.95 in. HO , PM
 Avg. Meter Temp. 102.8 F , TM 572.8

Moisture Collected

Empingers 151 Silica Gel 241
151 232
9
 Final vol. 302 Final wt. 241
 Initial vol. 200 Initial wt. 232
 Net vol. 102 Net wt. 9

Silica Gel 9 gm
 Empingers 9 ml
 Total Moisture 11 gm , VW

$$VM (std.) = \frac{17.65 \times VM \times Y \times [BP + (PM / 13.6)]}{(TM + 460)}$$

$$VW (gas) = 0.0471 \times VW = std. FT.$$

$$\% Moist. = \frac{100 \times VW (gas)}{VM (std.) + VW (gas)}$$

$$VM (std.) = \frac{17.65 \times 15.225 \times 1.03 \times [30.18 + (1.95 / 13.6)]}{(102.8 + 460)} = 19.830$$

$$VW (gas) = 0.0471 \times 11 = 0.518$$

$$\% Moist. = \frac{100 \times 0.518}{19.830 + 0.518} = \frac{51.8}{15.348} = 3.4\%$$

PARTICULATE FIELD DATA

Sheet 1 of 1
Client PECO

VERY IMPORTANT - FILL IN ALL BLANKS

Pitot Calibration

Read and record at the start of each test point

Thimble No. _____

BRITCH

Filter No. _____

% CO₂ 0.52 % O₂ 16.32

Ambient Temp. °F _____

Bar. Press. "Hg 29.8

Bar. Press. "Hg _____

16.4

Assumed Moisture % _____

Heater Box Setting, °F _____

Operator ALDRIGHT

Sample Box No. _____

Filter Box No. _____

Heater Δ _____

Probe Heater Setting _____

C Factor _____

Avg. ΔP _____

Avg. ΔE _____

POINT	DISTANCE IN INCHES	GLOBE TYPE	% O ₂ DRY GAS REFER. OR	PITOT IN. H ₂ O ΔP	ORIFICE Δ H IN. H ₂ O		DRY GAS TEMP. OF INLET	DRY GAS TEMP. OF OUTLET	PUMP VACUUM IN. Hg GAUGE	BOX TEMP. °F	IMPINGER TEMP. °F	STACK TEMP. °F
					DESIRED	ACTUAL						
1		0-0	16.6									
2			16.7									
3			16.6									
4			16.6									
5			16.5									
6			16.6									
7												
8												

Run No. UNIT 11 O₂-TRAVERSE

Location UNIT 11

Date 7/16/71

APPENDIX 4

RAW DATA

4.2 NO_x, MOISTURE, O₂ TRAVERSE - UNIT 21

GILBERT ASSOCIATES, INC.
ENGINEERS AND CONSULTANTS
READING, PA.

SUBJECT PECO

Cloydon Station

UNIT 21 Run 1

NO. PAGE

DATE 7/12/91

DATE

DATE

TEMP

TIME	METER	IN	OUT	DIFFER	VAC.
0844	0 408.8178	72	72	0	
1	5 408.825	79	79	0	
2	10	80	79	0	
3	15 408.996	180	79	0	
4	20 408.058	79	80	0	
5	25	82	82	0	
6	30 408.147	84	83	0	
7	35 408.228	85	84	0	
8	40 408.287	86	85	0	
9	45 408.341	85	82	0	
10	50 408.388	85	82	0	
11	55 408.444	88	82	0	
END	60 408.501				

TEMP	START	FINISH	NET	STOP	FINISH	NET
A				D		
B				E		
C						

GEL	START	FINISH	NET

0846
0946

Func
7062729
7066121

BAROMETER 29.98

STACK TEMP. 970

CONTROL BOX NO. 1385

$\gamma = 1.03$

Static +14.2' H₂O

OESAT

CO ₂		NET CO ₂
2.9	19.3	16.4
2.8	19.3	16.5
2.9	19.1	16.2
2.8	19.0	16.2

GILBERT ASSOCIATES, INC.
ENGINEERS AND CONSULTANTS
READING, PA.

CLIENT P E C O

Croydon

W.O. PAGE

99

NO. - 21 - 3

DATE 7/19/91

UNIT 2 Run 3

DATE

TIME	METER	IN	OUT	DIFFER	W.C.
START	0	409.250	96	95	0
1	5	409.300	95	95	0
2	10	409.390	96	95	0
3	15	+	99	96	0
4	20	+	99	97	0
5	25	409.552	99	97	0
6	30	409.580	99	97	0
7	35	409.627	100	98	0
8	40	409.660	100	99	0
9	45	409.741	100	99	0
10	50	409.800	100	100	0
11	55	409.872	100	100	0
END	60	409.931			

IMP	A	START	FINISH	NET	D	START	FINISH	NET
	B				E			
	C							

GEL	START	FINISH	NET
			1113

BAROMETER 29.99

STACK TEMP. 954

CONTROL BOX NO. 1385

Y = 1.03

ORSAT

CO ₂	NET O ₂
2.5	19.2
2.7	19.5
2.6	19.3
2.8	19.5

FUEL
7091300

7094812

APPENDIX 4

RAW DATA

4.3 NO_x, MOISTURE, O₂ TRAVERSE - UNIT 22

GILBERT ASSOCIATES, INC.
ENGINEERS AND CONSULTANTS
READING, PA.

CLIENT **PECO**

NOx-22-1

NO. PAGE
OF

UNIT 22 Run 1

7/18/91

Crowdon STATION

DATE

DATE

TIME	METERS	TEMP		REL. HUM.	WIND
		IN	OUT		
START 0930	0	422.946	85	84	0
1	5	422.980	85	84	0
2	10	422.065	85	85	0
3	15	422.130	82	82	0
4	20	422.192	89	88	0
5	25	422.268	91	88	0
6	30	422.338	92	89	10
7	35	422.410	93	90	0
8	40	422.480	94	92	0
9	45	422.543	94	93	0
10	50	422.610	95	94	0
11	55	422.675	96	94	0
END	60	422.744			

IMP	A	START	FINISH	NET	D	START	FINISH	NET
	B				E			
	C							

GEL	START	FINISH	NET

0937
1037

FUEL
4394179
4398833

BAROMETER 29.88

STACK TEMP. 979

CONTROL BOX NO. 1385

$\gamma = 1.03$

CORSAT

CO ₂	CO ₁	NET CO ₂
3.9	19.2	15.3
3.8	19.0	15.2
3.8	19.0	15.2
3.7	18.9	15.2

Static 16.5" H₂O

GILBERT ASSOCIATES, INC.
ENGINEERS AND CONSULTANTS
READING, PA.

CLIENT PECO

NOx-22-2

W.D. PAGE
OF

UNIT 22 Run 2
CROYDON STATION

2/18/91

DATE

DATE

	TIME	METHOD	IN	OUT	DIFFERENCE	VAC.
START	10:41	0	422.7210	96	75	0
1	5	422.8401	97	76	0	
2	10	422.899	97	76	0	
3	15	422.969	97	76	0	
4	20	428.029	98	77	0	
5	25	428.095	99	78	0	
6	30	428.160	100	79	0	
7	35	428.228	100	79	0	
8	40	428.289	100	79	0	
9	45	428.353	101	100	0	
10	50	428.420	102	101	0	
11	55	428.492	102	101	0	
END	60	428.563				

	START	FINISH	NET	START	FINISH	NET
IMP A				D		
B				E		
C						
GEL						

1043 4399310

BAROMETER 29.88

1143 4403082

STACK TEMP. 989

O2SAT

CONTROL BOX No. 1385

CO ₂	NET O ₂
3.8	18.8 15.0
3.8	19.0 15.2
3.9	19.1 15.2
3.9	18.9 15.0

$\gamma = 1.03$

Static +16.7" H₂O

GILBERT ASSOCIATES, INC.
ENGINEERS AND CONSULTANTS
READING, PA.

CLIENT *PECO*
Croydon Station

NO. PAGE
OF

UNIT 22 Run 3

DATE *7/18/97*

NOx-22-3

DATE

	TIME	METER	IN	OUT	DIFFER	VAC.
START	0	428.581	103	103	0	
1	5	428.640	104	104	0	
2	10	428.700	104	103	0	
3	15	428.770	104	104	0	
4	20	428.835	104	104	0	
5	25	428.905	105	105	0	
6	30	428.970	104	105	0	
7	35	429.035	105	105	0	
8	40	429.105	106	105	0	
9	45	429.182	106	106	0	
10	50	429.239	106	106	0	
11	55	429.300	106	106	0	
END	60	429.368				

	START	FINISH	NET	START	FINISH	NET
IMP A				D		
B				E		
C						

	START	FINISH	NET
GAL			

FUEL (Gallons)
1148
4404.263
1248
4408.740

BAROMETER *29.88*

STACK TEMP *975*

CONTROL BOX NO. *1385*

Y = 1.03

ORSAT

CO ₂		NET O ₂
3.5	18.8	15.3
3.6	18.8	15.2
3.5	18.8	15.3
3.5	18.8	15.2

Static + 16.3" H₂O

Date: 7/18/0

Moisture Determination

Run #: UN7 22

Point	Clock Actual	Time Run	Dry Gas Meter ft.	Orifice Pressure in. HO		Dry Gas Temp (F)	
				Inlet	Outlet	Inlet	Outlet
1	12.57	0.0	449.438	2.0	2.0	106	108
2		3.5	449.438	2.0	2.0	106	108
		7.0	449.438	2.0	2.0	106	108
3		10.5	449.438	2.0	2.0	106	108
		14.0	449.438	2.0	2.0	106	108
		17.5	449.438	2.0	2.0	106	108
		21.0	449.438	1.5	1.5	106	108

Y= Meter Factor = 1.03

Barometric Pressure: 29.88 in. Hg , BP
 Net Volume: _____ Cubic ft. , VM
 Avg. Orifice: _____ in. HO , PM
 Avg. Meter Temp. _____ F , TM

Moisture Collected

Impingers _____ Silica Gel _____

150

160

Final vol. 310 Final wt. 243
 Initial vol. 200 Initial wt. 239
 Net vol. 110 Net wt. 4

Silica Gel 4 gm
 Impingers 10 ml
 Total Moisture 14 gm , VW

$$VM (std.) = \frac{17.65 \times VM \times Y \times [BP + (PM / 13.6)]}{(TM + 460)}$$

$$VW (gas) = 0.0471 \times VW = std PP.$$

$$\% Moist. = \frac{100 \times VW (gas)}{VM (std.) + VW (gas)}$$

$$VM (std.) = \frac{17.65 \times \underline{110} \times \underline{1.03} \times [\underline{29.88} + (\underline{2.0} / 13.6)]}{(\underline{106} + 460)} = \underline{\hspace{2cm}}$$

$$VW (gas) = 0.0471 \times \underline{\hspace{2cm}} = \underline{\hspace{2cm}}$$

$$\% Moist. = \frac{100 \times \underline{\hspace{2cm}}}{\underline{\hspace{2cm}} + \underline{\hspace{2cm}}} = \underline{\hspace{2cm}}$$

APPENDIX 5

COMBUSTION CALCULATIONS FOR FLUE GAS FLOW

- 5.1 COMBUSTION CALCULATIONS - UNIT 11
- 5.2 COMBUSTION CALCULATIONS - UNIT 21
- 5.3 COMBUSTION CALCULATIONS - UNIT 22

APPENDIX 5

COMBUSTION CALCULATIONS FOR FLUE GAS FLOW

5.1 COMBUSTION CALCULATIONS - UNIT 11

UNIT 11 FUEL ANALYSIS
RUN 1

BTU/LB = 19370
 % ASH = 0.01
 % SULFUR = 0.14
 % CARBON = 86.90
 % H2 = 12.80
 %O2 = 0.14
 DENSITY(LBS/GAL)= 7.11
 GAL/HR = 3214

ORSAT INFORMATION

% O2 = 16.25
 % CO2 = 3.03
 % N2 = 80.73
 % CO = 0.00

%M = 3.4

FUEL CONSUMED(LBS/HR) = 22854.75
 EXCESS AIR = 321
 COMBUSTIBLES % = 0
 TEMP. = 971
 MOLECULAR WEIGHT OF GAS = 28.76
 MOLE FRACTION OF GAS = 0.966
 STACK PRESSURE = 31.18
 NOx Lbs/SCF = 2.56E-05
 MMBTU/HR = 443
 THEORETICAL AIR = 7.45
 UNBURNED FUEL LOSS = 0.00
 FUEL BURNED = 0.52
 DRY AIR = 31.38
 H2O IN AIR = 0.41
 WET GAS TOTAL = 32.30
 TOTAL FLUE GAS = 62.57
 DENSITY OF GAS = 0.0275
 TOTAL FLUE GAS FLOW = 866,768
 Qs (dscfm) = 323,186
 LBS/HR NOx = 497.20
 LBS NOx/MMBTU = 1.12

UNIT 11 FUEL ANALYSIS
RUN 2

BTU/LB = 19370
 % ASH = 0.01
 % SULFUR = 0.14
 % CARBON = 86.90
 % H2 = 12.80
 %O2 = 0.14
 DENSITY(LBS/GAL)= 7.11
 GAL/HR = 3210

ORSAT INFORMATION

% O2 = 15.40
 % CO2 = 3.03
 % N2 = 80.58
 % CO = 0.00

%M = 3.4

FUEL CONSUMED(LBS/HR) = 22826.31
 EXCESS AIR = 337
 COMBUSTIBLES % = 0
 TEMP. = 978
 MOLECULAR WEIGHT OF GAS = 28.76
 MOLE FRACTION OF GAS = 0.966
 STACK PRESSURE = 31.20
 NOx Lbs/SCF = 2.67E-05
 MMBTU/HR = 442
 THEORETICAL AIR = 7.45
 UNBURNED FUEL LOSS = 0.00
 FUEL BURNED = 0.52
 DRY AIR = 32.54
 H2O IN AIR = 0.42
 WET GAS TOTAL = 33.48
 TOTAL FLUE GAS = 64.85
 DENSITY OF GAS = 0.0274
 TOTAL FLUE GAS FLOW = 901,405
 Qs (dscfm) = 334,679
 LBS/HR NOx = 535.34
 LBS NOx/MMBTU = 1.21

UNIT 11 FUEL ANALYSIS
RUN 3

BTU/LB = 19370
% ASH = 0.01
% SULFUR = 0.14
% CARBON = 86.90
% H2 = 12.80
% O2 = 0.14
DENSITY (LBS/GAL)= 7.11
GAL/HR = 3074

ORSAT INFORMATION

% O2 = 16.63
% CO2 = 2.80
% N2 = 80.58
% CO = 0.00

WM = 3.4

FUEL CONSUMED(LBS/HR) = 21859.21
EXCESS AIR = 358
COMBUSTIBLES % = 0
TEMP. = 950
MOLECULAR WEIGHT OF GAS = 28.74
MOLE FRACTION OF GAS = 0.966
STACK PRESSURE = 31.20
NOx LBS/SCF = 2.32E-05
MMBTU/HR = 423
THEORETICAL AIR = 7.45
UNBURNED FUEL LOSS = 0.00
FUEL BURNED = 0.52
DRY AIR = 34.11
H2O IN AIR = 0.44
WET GAS TOTAL = 35.07
TOTAL FLUE GAS = 67.94
DENSITY OF GAS = 0.0279
TOTAL FLUE GAS FLOW = 887,562
Qs (cubic ft) = 336,084
LBS/HR NOx = 467.51
LBS NOx/MMBTU = 1.11

APPENDIX 5

COMBUSTION CALCULATIONS FOR FLUE GAS FLOW

5.2 COMBUSTION CALCULATIONS - UNIT 21

UNIT 21 FUEL ANALYSIS
RUN 1

BTU/LB = 19410
% ASH = 0.01
% SULFUR = 0.13
% CARBON = 87.00
% H2 = 12.50
% O2 = 0.25
DENSITY(LBS/GAL)= 7.11
GAL/HR = 3697

ORSAT INFORMATION

% O2 = 15.33
% CO2 = 2.85
% N2 = 80.88
% CO = 0.00

WM = 3.0

FUEL CONSUMED(LBS/HR) = 26289.37
EXCESS AIR = 326
COMBUSTIBLES % = 0
TEMP. = 970
MOLECULAR WEIGHT OF GAS = 28.78
MOLE FRACTION OF GAS = 0.970
STACK PRESSURE = 31.02
NOx Lbs/SCF = 2.56E-05
MMBTU/HR = 510
THEORETICAL AIR = 7.40
UNBURNED FUEL LOSS = 0.00
FUEL BURNED = 0.52
DRY AIR = 31.52
H2O IN AIR = 0.41
WET GAS TOTAL = 32.44
TOTAL FLUE GAS = 62.97
DENSITY OF GAS = 0.028
TOTAL FLUE GAS FLOW = 1.00E+06
Gs (dscfm) = 373,508
LBS/HR NOx = 573.54
LBS NOx/MMBTU = 1.12

UNIT 21 FUEL ANALYSIS
RUN 2

BTU/LB = 19410
% ASH = 0.01
% SULFUR = 0.13
% CARBON = 87.00
% H2 = 12.50
% O2 = 0.25
DENSITY(LBS/GAL)= 7.11
GAL/HR = 3588

ORSAT INFORMATION

% O2 = 16.40
% CO2 = 2.73
% N2 = 80.88
% CO = 0.00

WM = 3.0

FUEL CONSUMED(LBS/HR) = 25514.27
EXCESS AIR = 331
COMBUSTIBLES % = 0
TEMP. = 960
MOLECULAR WEIGHT OF GAS = 28.76
MOLE FRACTION OF GAS = 0.970
STACK PRESSURE = 31.01
NOx Lbs/SCF = 2.43E-05
MMBTU/HR = 495
THEORETICAL AIR = 7.40
UNBURNED FUEL LOSS = 0.00
FUEL BURNED = 0.52
DRY AIR = 31.92
H2O IN AIR = 0.41
NET GAS TOTAL = 32.85
TOTAL FLUE GAS = 63.76
DENSITY OF GAS = 0.028
TOTAL FLUE GAS FLOW = 9.78E+05
Gs (dscfm) = 367,106
LBS/HR NOx = 536.15
LBS NOx/MMBTU = 1.08

UNIT 21 FUEL ANALYSIS
RUN 3

BTU/LB = 19410
% ASH = 0.01
% SULFUR = 0.13
% CARBON = 87.00
% H2 = 12.60
NO2 = 0.25
DENSITY(LBS/GAL)= 7.11
GAL/HR = 3512

ORSAT INFORMATION
% O2 = 16.73
% CO2 = 2.55
% H2 = 80.63
% CO = 0.00

W = 3.0

FUEL CONSUMED (LBS/HR) = 24973.83
EXCESS AIR = 367
COMBUSTIBLES % = 0
TEMP. = 954
MOLECULAR WEIGHT OF GAS = 28.76
MOLE FRACTION OF GAS = 0.970
STACK PRESSURE = 31.02
NOx LBS/SCF = 2.26E-05
MMBTU/HR = 485
THEORETICAL AIR = 7.40
UNBURNED FUEL LOSS = 0.00
FUEL BURNED = 0.52
DRY AIR = 34.55
H2O IN AIR = 0.45
WET GAS TOTAL = 35.51
TOTAL FLUE GAS = 68.93
DENSITY OF GAS = 0.028
TOTAL FLUE GAS FLOW = 1.03E+06
Gs (dscfm) = 388,583
LBS/HR NOx = 527.63
LBS NOx/MMBTU = 1.09

APPENDIX 5

COMBUSTION CALCULATIONS FOR FLUE GAS FLOW

5.3 COMBUSTION CALCULATIONS - UNIT 22

UNIT 22 FUEL ANALYSIS
RUN 1

BTU/LB = 19360
% ASH = 0.01
% SULFUR = 0.12
% CARBON = 86.90
% H2 = 12.60
%O2 = 0.38
DENSITY(LBS/GAL)= 7.13
GAL/HR = 4654

ORSAT INFORMATION

% O2 = 15.23
% CO2 = 3.80
% N2 = 80.98
% CO = 0.00

SM = 4.1

FUEL CONSUMED(LBS/HR) = 33173.71
EXCESS AIR = 247
COMBUSTIBLES % = 0
TEMP. = 979
MOLECULAR WEIGHT OF GAS = 28.76
MOLE FRACTION OF GAS = 0.959
STACK PRESSURE = 31.09
NOx Lbs/SCF = 1.50E+05
MMBTU/HR = 642
THEORETICAL AIR = 7.41
UNBURNED FUEL LOSS = 0.00
FUEL BURNED = 0.52
DRY AIR = 25.76
H2O IN AIR = 0.33
WET GAS TOTAL = 26.61
TOTAL FLUE GAS = 51.52
DENSITY OF GAS = 0.027
TOTAL FLUE GAS FLOW = 1.04E+06
Qs (dscfm) = 382,376
LBS/HR NOx = 344.71
LBS NOx/MMBTU = 0.54

UNIT 22 FUEL ANALYSIS
RUN 2

BTU/LB = 19360
% ASH = 0.01
% SULFUR = 0.12
% CARBON = 86.90
% H2 = 12.60
%O2 = 0.38
DENSITY(LBS/GAL)= 7.13
GAL/HR = 4677

ORSAT INFORMATION

% O2 = 15.13
% CO2 = 3.85
% N2 = 81.05
% CO = 0.00

SM = 4.1

FUEL CONSUMED(LBS/HR) = 32624.86
EXCESS AIR = 240
COMBUSTIBLES % = 0
TEMP. = 987
MOLECULAR WEIGHT OF GAS = 28.76
MOLE FRACTION OF GAS = 0.959
STACK PRESSURE = 31.11
NOx Lbs/SCF = 1.54E+05
MMBTU/HR = 632
THEORETICAL AIR = 7.41
UNBURNED FUEL LOSS = 0.00
FUEL BURNED = 0.52
DRY AIR = 25.18
H2O IN AIR = 0.33
WET GAS TOTAL = 26.03
TOTAL FLUE GAS = 50.39
DENSITY OF GAS = 0.027
TOTAL FLUE GAS FLOW = 1.01E+06
Qs (dscfm) = 367,946
LBS/HR NOx = 340.25
LBS NOx/MMBTU = 0.54

UNIT 22 FUEL ANALYSIS
RUN 3

BTL/LB = 193.60
% ASH = 0.01
% SULFUR = 0.12
% CARBON = 86.90
% H2 = 12.60
% O2 = 0.38
DENSITY (LBS/GAL) = 7.13
GAL/HR = 44.77

ORSAT INFORMATION

% O2 = 15.25
% CO2 = 3.53
% N2 = 81.23
% CO = 0.00

SM = 4.1

FUEL CONSUMED (LBS/HR) = 31912.06
EXCESS AIR = 24.6
COMBUSTIBLES % = 0
TEMP. = 975
MOLECULAR WEIGHT OF GAS = 28.72
MOLE FRACTION OF GAS = 0.959
STACK PRESSURE = 31.08
NOx LBS/SCF = 1.56E+05
MMBTU/HR = 618
THEORETICAL AIR = 7.41
UNBURNED FUEL LOSS = 0.00
FUEL BURNED = 0.52
DRY AIR = 25.66
H2O IN AIR = 0.33
WET GAS TOTAL = 26.51
TOTAL FLUE GAS = 51.32
DENSITY OF GAS = 0.027
TOTAL FLUE GAS FLOW = 9.97E+05
Qs (dscfm) = 366,803
LBS/HR NOx = 343.34
LBS NOx/MMBTU = 0.56

APPENDIX 6
LABORATORY RESULTS

- 6.1 NO_x ANALYSIS
- 6.2 CO ANALYSIS
- 6.3 FUEL ANALYSIS

APPENDIX 6

LABORATORY RESULTS

6.1 NO_x ANALYSES



ROY F. WEBSTON, INC.
Lionville Laboratory

CLIENT: GILBERT ASSOCIATES, INC
RFW #: 9107L202
W.O. #: 3494-02-01

SAMPLES RECEIVED: 07-18-91

INORGANIC NARRATIVE

The following is a summary of the quality control results and a description of any problems encountered during the analysis of this batch of samples:

1. All preparation blank results were below the required detection limit.
2. All laboratory control standards (blank spikes) were within the control limits of 80-120%.
3. All calibration verification checks are within the required control limits of 90-110%. Calibration verification is performed using independent standards.
4. The analytical methods applied by the laboratory, unless otherwise requested, for all inorganic analyses are derived from the USEPA Method for Chemical Analysis of Water and Wastes (USEPA 600/4-79-020), and Standard Methods for the Examination of Water and Wastewater 16 ed. Methods for the analysis of solid samples are derived from Test Methods for Evaluating Solid Waste (USEPA SW846).

Jack R. Tuschall, Ph.D.
Laboratory Manager
Lionville Analytical Laboratory

8.23.91

Date

ROY P. WESTON INC.

INORGANICS DATA SUMMARY REPORT 08/20/91

CLIENT: GILBERT ASSOCIATES, INC
 WORK ORDER: 3494--02--01--0000

WESTON BATCH #: 9107L202

SAMPLE	SITE ID	ANALYTE	RESULT	UNITS	REPORTING LIMIT
--001	NOK11--1	NOK	8220	ug NOK	464
--002	NOK21--1	NOK	8190	ug NOK	464
--003	NOK22--1	NOK	5580	ug NOK	464
--004	BLANK	NOK	464	u ug NOK	464
--005	SPIKE (DER)	NOK ^{2.6} <i>2.6 ug by (Bocum) (PVC) 320 ug (Bocum) 6-1 Hand</i>	2560	ug NOK	232
--006	NOK11--2	NOK	7800	ug NOK	464
--007	NOK11--3	NOK	7920	ug NOK	464
--008	NOK21--2	NOK	8130	ug NOK	464
--009	NOK21--3	NOK	6930	ug NOK	464
--010	NOK22--2	NOK	5600	ug NOK	464
--011	NOK22--3	NOK	5550	ug NOK	464

ROY P. WESTON INC.

INORGANICS METHOD BLANK DATA SUMMARY PAGE 06/20/91

CLIENT: GILBERT ASSOCIATES, INC
 WORK ORDER: 3494--02--01--0000

WESTON BATCH #: 91071202

SAMPLE	SITE ID	ANALYTE	RESULT	UNITS	REPORTING LIMIT
BLANK10	91LIC125-MB1	NOX	464	u. ug NOX	464
BLANK10	91LIC129-MB1	NOX	464	u. ug NOX	464

ROY F. WESTON INC.

INORGANICS ACCURACY REPORT 08/20/91

CLIENT: GILBERT ASSOCIATES, INC
 WORK ORDER: 3494-02-01-0000

WESTON BATCH #: 91071202

SAMPLE	SITE ID	ANALYTE	SPIKED SAMPLE	INITIAL RESULT	SPIKED AMOUNT	%RECOV
BLANK10	91LIC125-MB1	NOX	18900	464	18500	102
BLANK10	91LIC129-MB1	NOX	19800	464	18500	107

Custody Transfer Record/Lab Work Request

WESTON Analyticals Use Only
 9107L2002

Client: Colbert Community
 Est. Final Proj. Sampling Date: 7/1/91
 Work Order #: 600-00-00
 Project Contact/Phone #: 78-2600 Ext 1116
 AD Project Manager: Earl R. Ruffalo
 CC S.M. Del: SAI TAT AI
 Date Rec'd: 7/1/91 Date Due: 8/1/91
 Account #: 618/310

Lab ID	Client ID/Description	Matrix Chosen (M)	Matrix Collected	Date Collected	ANALYSES REQUESTED	ORGANIC	YOR	BNR	PERL	TCR	TCF
001	ALX 11-1 2-3 9/1/91	Q	Q	7/1/91							
002	ALX 11-1 2-3 9/1/91	Q	Q	7/1/91							
003	ALX 11-1 2-3 9/1/91	Q	Q	7/1/91							
004	BLANK			7/1/91							
005	SPIKE (DEC)			7/1/91							

Special Instructions: EPA METHOD 7D-NOx Analysis
* Analyze Spike Sample Also

DATE REVISIONS:
 1. Dec 1990
 2. Dec 006-Oil added
 3. Matrix ID's changed
 4. _____
 5. _____
 6. _____

WESTON Analyticals Use Only

Samples were:
 1) Shipped Y or N
 2) Unbroken on Arrival Y or N
 3) Received in Good Condition Y or N
 4) Properly preserved Y or N
 5) Received within Holding Time Y or N
 6) Received Present Upon Sample Receipt Y or N

Discrepancies Between Samples Labels and COC Record? Y or N

NOTES:



Custody Transfer Record/Lab Work Request

WESTON Analytics Use Only

91071202

Client

Work Order

Date Rec'd

RFW Contact

Client Contact/Phone

Client ID/Description

Matrix

Item/Reason

Time

Date

Received by

Item/Reason

Time

Date

Received by

Special instructions

W - Water

S - Soil

SE - Sediment

SO - Solid

DS - Drum Solids

DL - Drum Liquids

A - Air

W - Wipe

L - EPIC/CL Leachate

X - Other

Item/Reason

Time

Date

Received by

Item/Reason

Time

Date

Received by

Discrepancies Between Sample Labels and COC Record?

Y N

NOTES

WESTON Analytics Use Only

Samples Were:

1 Shipped or Hand-Delivered

NOTES:

2 Ambient or Chilled

NOTES:

3 Received Broken/Leaking (Improperly Sealed)

Y N

NOTES:

4 Properly Preserved

Y N

NOTES:

5 Received Within Holding Times

Y N

NOTES:

COC Tapes Was:

1 Present on Outer Package

Y N

2 Unbroken on Outer Package

Y N

3 Present on Sample

Y N

4 Unbroken on Sample

Y N

NOTES:

COC Fingerprint Was:

1 Present Upon Receipt of Samples

Y N

Discrepancies Between Sample Labels and COC Record?

Y N

NOTES:

APPENDIX 6

LABORATORY RESULTS

6.2 CO ANALYSIS



WESTON WAY
WEST CHESTER, PA 19380
PHONE: 215-692-3030
TELEX: 83-5348

12 August 1991

Gilbert Commonwealth
P.O. Box 1498
Reading, PA 19603

Attention: Mr. Steve Foulk
Subject: Carbon Monoxide Analysis

Dear Mr. Foulk:

The results of the carbon monoxide analysis performed on the set of nine Tedlar® gas sample bags delivered in lots of 3 to WESTON on July 16, 17 and 18, 1991 are outlined below and support data is attached.

The analysis was performed according to EPA Method 10B. No problems were encountered with the samples delivered and analyzed on July 16. Background noise levels increased during analysis of the July 17 and 18 samples. The lowest detectable limit was 0.5 ppm CO. Multiple injections were conducted for each bag and the average of three runs was calculated.

Very truly yours,

ROY F. WESTON, INC.

Jeffrey D. O'Neill
Senior Section Manager

JDO/mb

DATA SUMMARY

SAMPLE NO.	DATE	CONCENTRATION PPMV
CO-11-1	7/16	1.2
CO-11-2	7/16	1.3
CO-11-3	7/16	1.5
CO-21-1	7/17	0.9
CO-21-2	7/17	0.9
CO-21-3	7/17	0.9
CO-22-1	7/18	0.9
CO-22-2	7/18	1.1
CO-22-3	7/18	1.5

EPA METHOD 10B
CARBON MONOXIDE ANALYSIS
7/16/91

SAMPLE	PEAK AREA	AUG. PEAK AREA	CONCENTRATION PPMV RESPONSE FACTOR ¹
24.9 ppm CO	13,731 13,941 14,392	14,021	1.776×10^{-3}
252 ppm CO	155,398 151,663 155,047	154,036	1.636×10^{-3}
CO-11-1	576 653 742	657	1.2
CO-11-2	670 783	727	1.3
CO-11-3	619 960 971	850	1.5
24.9 ppm CO	14,187		1.755×10^{-6}

¹ Used 1.765×10^{-3} average response factor.

EPA METHOD 10B
CARBON MONOXIDE ANALYSIS
7/17-18/91

SAMPLE	PEAK AREA	AUG. PEAK AREA	CONCENTRATION PPMV RESPONSE FACTOR ¹
24.9 ppm CO	14,735 15,389 14,641 16,282	15,262	1.632×10^{-3}
49.4 ppm CO	29,397 30,148 31,762	30,436	1.623×10^{-3}
CO-21-3	657 508 687	617	0.9
CO-21-2	700 407 755 538	600	0.9
CO-21-1	397 575 858	610	0.9
24.9 ppm CO	17,229	17,229	1.445×10^{-3}
CO-22-1	444 824 613	627	0.9
CO-22-3	1,781 657 717	1,052	1.5
CO-22-2	976 809 605	797	1.1
24.9 ppm CO	19,549 17,557	18,553	1.342×10^{-3}
49.4 ppm CO	33,671 34,433 35,272	34,458	1.434×10^{-3}

¹ Used 1.536×10^{-3} for CO-21.
 1.407×10^{-3} for CO-22

APPENDIX 6

LABORATORY RESULTS

6.3 FUEL ANALYSIS



REQUEST FOR LABORATORY ANALYTICAL SERVICES

106721

Client Name: GIC

Address: _____

Spotts, Stevens & McCoy Report to: Steve Falch

EQI No: _____

W.O. No: _____

Phone Report Request: _____

FACR Report: _____

Requested Reporting Date: _____

Lab Approval: _____
Priority charges authorized by client: _____

Project Description: oil - prep Sampled By: client Date/Time: 7/17/91

CLIENT SAMPLE ID	# OF CONTAINERS	SAMPLE DESCRIPTION	ANALYSIS REQUESTED
Unit # 11			BTU lbb - gal.
" # 21	19260		API - density Ash Sulph
" # 22			Carbon Hydrogen
			Oxygen

CHAIN OF CUSTODY

Delivery to laboratory
Custody relinquished by: [Signature]
To: Vaughn [Signature] Date: 7/19/91 Time: 2:00

Intralaboratory Transfer
Custody relinquished by: [Signature] 127920
To: _____ Date: _____ Time: _____

Custody relinquished by: _____
To: _____ Date: _____ Time: _____

Custody relinquished by: _____
To: _____ Date: _____ Time: _____

Custody relinquished by: _____
To: _____ Date: _____ Time: _____

Comments/Special Requests: _____

ANALYTICAL REPORT

CLIENT: Steve Folk
 Gilbert/Commonwealth, Inc.
 P. O. Box 1498
 Reading PA 19603

PROJECT: 106721
 PO NO: 52850
 REPORTED: 29-JUL-91
 RECEIVED: 19-JUL-91
 WORK ORDER:

PROJECT DESCRIPTION: Oil Peco

SAMPLING DATE: 17-JUL-91 BY: Client

	UNITS	RESULT
SAMPLE: 1025780		
UNIT #11		
Heating Value	BTU/lb	19370
Gravity, API		34.2
Ultimate Analysis		
CHN Analysis		
Carbon	%	86.9
Hydrogen	%	12.8
Nitrogen	%	< 0.02
Oxygen	%	0.14
Ash	%	< 0.01
Sulfur	%	0.14

< Indicates less than value.

Density (lbs/gal) = 7.111

Heating Value (Btu/gal) = 137710

SAMPLE: 1025781		
UNIT #21		
Heating Value	BTU/lb	19410
Gravity, API		34.2

Ultimate Analysis		
CHN Analysis		
Carbon	%	87.0
Hydrogen	%	12.6
Nitrogen	%	< 0.02
Oxygen	%	0.25
Ash	%	< 0.01
Sulfur	%	0.13

< Indicates less than value.

Density (lbs/gal) = 7.111

Heating Value (Btu/gal) = 138010



CLIENT: Gilbert/Commonwealth, Inc.
PROJECT: 106721

Page 2
29-JUL-91

SAMPLE: 1025782

UNIT #22

Heating Value

BTU/lb

19360

Gravity, API

33.8

Ultimate Analysis

CHN Analysis

Carbon	%	86.9
Hydrogen	%	12.6
Nitrogen	%	< 0.02
Oxygen	%	0.38
Ash	%	< 0.01
Sulfur	%	0.12

< Indicated less than value.

Density (lb/gal) = 7.128

Heating Value (Btu/gal) = 137970

Respectfully submitted,

A handwritten signature in cursive script, reading "Vaughan J. O'Neill".

Vaughan J. O'Neill,
Group Leader, Physical Testing

APPENDIX 7

COMPUTER PRINTOUTS

- 7.1 NO_x, MOISTURE, CO - UNIT 11
- 7.2 NO_x, MOISTURE, CO - UNIT 21
- 7.3 NO_x, MOISTURE, CO - UNIT 22

APPENDIX 7

COMPUTER PRINTOUTS

7.1 NO_x, MOISTURE, CO - UNIT 11

GILBERT/COMMONWEALTH, INC.
 TESTING SERVICES GROUP

NOX EMISSIONS

CLIENT: PECCO

W.O. NO.: 04-6314-000

TEST: NO-11-1 DATE: 7/16/91 START TIME: 1014 END TIME: 1114

OPERATOR: ALBRIGHT

VM = 0.688 TN = 90 PPM = 214.7 VMSD = 0.586 NO2(CMG) = 8220.0
 NOx, LBS/SCF = 2.56E-05 %N = 3.4 BP = 30.17 CONC(MG/DSCM) = 410.595
 DSCFM = 323,186 Y(METER) = 1.03

TIME PER READING	METER	TEMPERATURE INLET	TEMPERATURE OUTLET	ORIFICE	O2	CO2
5	390.330	79	81	0		
5		86	85	0	16.0	3.0
5		87	85	0		
5		88	87	0		
5		89	88	0	16.5	3.3
5		91	89	0		
5		92	90	0		
5		93	91	0	16.1	2.9
5		94	92	0		
5		95	93	0		
5		94	93	0		
5	391.018	94	93	0	16.4	2.9

TIME	VM	TN	OR	O2	CO2
60	0.688	90	0	16.3	3.0

EMISSIONS

DRY:

PPM, NOX = 214.7 MMBTU/HR = 463.0
 LBS/HR = 497.20
 LBS/MMBTU = 1.122

GILBERT/COMMONWEALTH, INC.
TESTING SERVICES GROUP

NOX EMISSIONS

CLIENT: PECO

W.O. NO.: 04-5314-000

TEST: NO-11-2 DATE: 7/16/91 START TIME: 1137 END TIME: 1237

OPERATOR: ALBRIGHT

VM = 0.535 TN = 97 PPM = 223.3 VMSTD = 0.626 NO2(ug) = 7800.0
 NOx, Lbs/SCF = 2.167E-05 XM = 3.4 BP = 30.18 CONC(mg/DSCM) = 426.909
 DSCFM = 334,679 Y(METER) = 1.03

TIME PER READING	METER	TEMPERATURE INLET	TEMPERATURE OUTLET	ORIFICE	O2	CO2
5	391.047	95	93	0		
5		95	94	0	16.5	2.8
5		95	95	0		
5		97	96	0		
5		98	96	0	16.4	2.9
5		98	96	0		
5		98	96	0		
5		98	97	0	16.4	3.1
5		99	97	0		
5		97	97	0		
5		98	97	0		
5	391.682	99	98	0	16.3	3.3

TIME	VM	TN		OR	O2	CO2
60	0.635	97		0	16.4	3.0

EMISSIONS

DRY:
 PPM, NOX = 223.3 MMBTU/HR = 462.0
 LBS/HR = 535.34
 LBS/MMBTU = 1.211

GILBERT/COMMONWEALTH, INC.
 TESTING SERVICES GROUP

NOX EMISSIONS

CLIENT: PECC

W.O. NO.: 06-5314-000

TEST: NOX-11-3 DATE: 7/16/91 START TIME: 1255 END TIME: 1355

OPERATOR: ALBRIGHT

VM = 0.748 TN = 101 PPM = 194.2 VMSTD = 0.732 NO2(ug) = 7920.0
 NOx, Lbs/SCF = 2.32E-05 WM = 3.4 BP = 30.18 CONC(mg/DSCM) = 371.254
 DSCFM = 336,084 Y(METER) = 1.03

TIME PER READING	METER	TEMPERATURE INLET	TEMPERATURE OUTLET	ORIFICE	O2	CO2
5	391.714	99	98	0	16.6	2.9
5		99	98	0		
5		100	99	0		
5		101	100	0		
5		101	100	0	16.3	2.7
5		101	100	0		
5		102	101	0		
5		102	101	0		
5		102	101	0	16.8	2.8
5		101	100	0		
5		101	100	0		
5	392.462	101	100	0	16.8	2.8

TIME	VM	TN	OR	O2	CO2
60	0.748	101	0	16.6	2.8

EMISSIONS

DRY:
 PPM, NOX = 194.2 MMBTU/HR = 623.0
 LBS/HR = 467.51
 LBS/MMBTU = 1.105

GILBERT/COMMONWEALTH, INC.
TESTING SERVICES GROUP

FIELD MOISTURE DETERMINATION

CLIENT: PECCO

N.O. NO.: 6314-000

TEST: N-11-1 DATE: 7/16/91 TIME: 1400

OPERATOR: ALBRIGHT

BAROMETRIC PRESSURE: 30.18

GAS METER

START: 392.538 FINAL: 407.813 NET: 15.275

Y FACTOR: 1.03

FLOW METER

AVE. ORIFICE DROP: 1.95 AVE. TEMPERATURE: 108

MOISTURE

IMP 1	START:	150	FINAL:	151	NET:	1
IMP 2	START:	150	FINAL:	151	NET:	1
IMP 3	START:	0	FINAL:	0	NET:	0
GEL	START:	232	FINAL:	241	NET:	9

TOTAL COLLECTED MOISTURE: 11.0

TOTAL MOISTURE BY WEIGHT: 3.4 %

SAMPLE VOLUME (VMSTD): 14.825

GILBERT/COMMONWEALTH, INC.
 TESTING SERVICES GROUP

CO EMISSIONS

CLIENT: PHILADELPHIA ELECTRIC COMPANY

LOCATION: CROYDON STATION

UNIT 11	LAB RESULTS CO, PPM BAG SAMPLE	% CO2 IN STACK	CO, PPM, DRY BASIS CORRECTED FOR CO2	CO LBS/SEC	FLOW DSCFH	CO LBS/HR	MMBTU/HR	CO LBS/MMBTU
RUN 1	1.20	3.03	1.16	8.49E-08	323,185	1.62	443	0.00372
RUN 2	1.30	3.03	1.26	9.20E-08	334,679	1.85	442	0.00418
RUN 3	1.50	2.80	1.46	1.06E-07	336,084	2.15	423	0.00507

APPENDIX 7

COMPUTER PRINTOUTS

7.2 NO_x, MOISTURE, CO - UNIT 21

GILBERT/COMMONWEALTH, INC.
 TESTING SERVICES GROUP

NOX EMISSIONS

CLIENT: PECC

W.O. NO.: 06-6314-000

TEST: NOX-21-1 DATE: 7/17/91 START TIME: 844 END TIME: 944

OPERATOR: ALBRIGHT

VM = 0.683 TN = 83 PPM = 214.3 VMSTD = 0.686 NO2(ug) = 8190.0
 NOx, Lbs/SCF = 2.56E-05 SM = 3.0 BP = 29.98 CONC(mg/DSCM) = 409.826
 DSCFM = 373,508 Y(METER) = 1.03

TIME PER READING	METER	TEMPERATURE INLET	TEMPERATURE OUTLET	ORIFICE	O2	CO2
5	407.818	77	77	0	16.4	2.9
5		79	79	0		
5		80	79	0		
5		80	79	0		
5		79	80	0	16.5	2.8
5		82	82	0		
5		85	83	0		
5		85	84	0		
5		86	85	0	16.2	2.9
5		85	87	0		
5		85	87	0		
5	408.501	88	87	0	16.2	2.8

TIME	VM	TN	OR	O2	CO2	
60	0.683	83	0	16.3	2.9	

EMISSIONS

DRY:

PPM, NOX = 214.3 MMBTU/HR = 510.0
 LBS/HR = 573.54
 LBS/MMBTU = 1.125

GILBERT/COMMONWEALTH, INC.
 TESTING SERVICES GROUP

NOX EMISSIONS

CLIENT: PECO

W.O. NO.: 04-6314-000

TEST: NOX-21-2 DATE: 7/17/91 START TIME: 958 END TIME: 1058

OPERATOR: ALBRIGHT

VN = 0.725 TN = 92 PPM = 203.9 VNSTD = 0.716 NO2(ug) = 8130.0
 NOx, Lbs/SCF = 2.43E-05 WM = 3.1 BP = 30.00 CONC(mg/DSCM) = 389.785
 DSCFM = 367,106 Y(METER) = 1.03

TIME PER READING	METER	TEMPERATURE INLET	TEMPERATURE OUTLET	ORIFICE	O2	CO2
5	408.526	90	89	0	16.3	2.9
5		90	89	0		
5		90	89	0		
5		90	89	0		
5		91	89	0	16.5	2.7
5		92	91	0		
5		93	91	0		
5		93	92	0		
5		94	93	0	16.5	2.6
5		94	93	0		
5		95	95	0		
5	409.251	95	94	0	16.3	2.7

TIME	VN	TN	OR	O2	CO2	
60	0.725	92	0	16.4	2.7	

EMISSIONS

DRY:
 PPM, NOX = 203.9 MMBTU/HR = 695.0
 LBS/HR = 536.15
 LBS/MMBTU = 1.083

GILBERT/COMMONWEALTH, INC.
TESTING SERVICES GROUP

NOX EMISSIONS

CLIENT: PECO

W.O. NO.: 04-6314-000

TEST: NOX-21-3 DATE: 7/17/91 START TIME: 1112 END TIME: 1212

OPERATOR: ALBRIGHT

VM = 0.673 TM = 98 PPM = 189.5 VMSTD = 0.657 NO2 (ug) = 6930.0
 NOX, Lbs/SCF = 2.26E-05 XM = 3.1 BP = 29.99 CONC (mg/DSCFM) = 362.392
 DSCFM = 388,583 YC (METER) = 1.03

TIME PER READING	METER	TEMPERATURE INLET	TEMPERATURE OUTLET	ORIFICE	O2	CO2
5	409.258	96	95	0	16.7	2.5
5		95	95	0		
5		96	95	0		
5		99	96	0		
5		99	97	0	16.8	2.7
5		99	97	0		
5		99	97	0		
5		100	98	0		
5		100	99	0	16.7	2.6
5		100	99	0		
5		100	100	0		
5	409.931	100	100	0	16.7	2.8

TIME	VM	TM	OR	O2	CO2	
60	0.673	98	0	16.7	2.7	

EMISSIONS

DRY:

PPM, NOX = 189.5 MMBTU/HR = 485.0
 LBS/HR = 527.63
 LBS/MMBTU = 1.088

GILBERT/COMMONWEALTH, INC.
TESTING SERVICES GROUP

FIELD MOISTURE DETERMINATION

CLIENT: PECC

W.O. NO.: 6314-000

TEST: N21-1 DATE: 7/17/91 TIME: 1235

OPERATOR: ALBRIGHT

BAROMETRIC PRESSURE: 29.97

GAS METER

START: 410.066 FINAL: 426.933 NET: 16.867

Y FACTOR: 1.03

FLOW METER

AVE. ORIFICE DROP 2.00 AVE. TEMPERATURE: 96

MOISTURE

DMP 1 START: 150 FINAL: 152 NET: 2

DMP 2 START: 150 FINAL: 152 NET: 2

DMP 3 START: 0 FINAL: 0 NET: 0

GEL START: 232 FINAL: 239 NET: 7

TOTAL COLLECTED MOISTURE: 11.0

TOTAL MOISTURE BY WEIGHT: 3.0 %

SAMPLE VOLUME(CM3STD): 16.601

GILBERT/COMORHEALTH, INC.
 TESTING SERVICES GROUP

CO EMISSIONS

CLIENT: PHILADELPHIA ELECTRIC COMPANY

LOCATION: CROYDON STATION

UNIT 21	LAB RESULTS CO, PPM BIG SAMPLE	X CO2 IN STACK	CO, PPM, DRY BASIS CORRECTED FOR CO2	CO LBS/SEC	FLOW SCFH	CO LBS/HR	MMBTU/HR	CO LBS/MMBTU
RUN 1	0.90	2.85	0.87	6.38E-08	373,508	1.43	510	0.00290
RUN 2	0.90	2.73	0.86	6.39E-08	367,264	1.41	495	0.00284
RUN 3	0.90	2.65	0.86	6.40E-08	360,751	1.49	485	0.00308

APPENDIX 7

COMPUTER PRINTOUTS

7.3 NO_x, MOISTURE, CO - UNIT 22

GILBERT/COMMONWEALTH, INC.
 TESTING SERVICES GROUP

NOX EMISSIONS

CLIENT: PECC

W.O. NO.: 04-6316-000

TEST: NOX-22-1 DATE: 7/18/91 START TIME: 934 END TIME: 1034

OPERATOR: ALBRIGHT

VM = 0.798 TM = 90 PPM = 125.8 VMSTD = 0.788 NO2(ug) = 5580.0
 NOx, Lbs/SCF = 1.50E-05 XM = 4.1 BP = 29.88 CONC(mg/DSCM) = 240.598
 DSCFM = 382,376 Y(METER) = 1.03

TIME PER READING	METER	TEMPERATURE INLET	TEMPERATURE OUTLET	ORIFICE	O2	CO2
5	426.946	85	84	0	15.3	3.9
5		85	84	0		
5		85	85	0		
5		87	87	0		
5		89	88	0	15.2	3.8
5		91	88	0		
5		92	89	0		
5		93	90	0		
5		94	92	0	15.2	3.8
5		94	93	0		
5		95	94	0		
5	427.744	96	94	0	15.2	3.7

TIME	VM	TM	OR	O2	CO2	
60	0.798	90	0	15.2	3.8	

EMISSIONS

DRY:
 PPM, NOX = 125.8 MMBTU/HR = 642.0
 LBS/HR = 344.71
 LBS/MMBTU = 0.537

GILBERT/COMMONWEALTH, INC.
 TESTING SERVICES GROUP

NOX EMISSIONS

CLIENT: PECO

W.D. NO.: 04-6314-000

TEST: NOX-22-2 DATE: 7/18/91 START TIME: 1041 END TIME: 1144

OPERATOR: ALBRIGHT

VM = 0.793 TN = 99 PPM = 129.1 VMSTD = 0.771 NO2 (ug) = 5600.0
 NOX, Libb/SCF = 1.54E+05 SM = 4.3 BP = 29.88 CONC(ng/DSCM) = 246.797
 DSCFM = 367,966 YCMETER = 1.03

TIME PER READING	METER	TEMPERATURE INLET	TEMPERATURE OUTLET	ORIFICE	O2	CO2
5	427.770	96	95	0	15.0	3.8
5		97	96	0		
5		97	96	0		
5		97	96	0		
5		98	97	0	15.2	3.8
5		99	98	0		
5		100	99	0		
5		100	99	0		
5		100	99	0	15.2	3.9
5		101	100	0		
5		102	101	0		
5	428.563	102	101	0	15.0	3.7

TIME	VM	TN	OR	O2	CO2
60	0.793	99	0	15.1	3.8

EMISSIONS

DRY:
 PPM, NOX = 129.1 MMBTU/HR = 632.0
 LIBS/HR = 340.25
 LIBS/MMBTU = 0.538

GILBERT/COMMONWEALTH, INC.
 TESTING SERVICES GROUP

NOX EMISSIONS

CLIENT: PECC

W.O. NO.: 06-6314-000

TEST: NOX-22-3 DATE: 7/18/91 START TIME: 1147 END TIME: 1247

OPERATOR: ALBRIGHT

VM = 0.787 TM = 105 PPM = 130.7 MVSTD = 0.757 NO2 (ug) = 5550.0
 NOx, Lbs/SCF = 1.56E-05 SM = 4.3 BP = 29.88 CONC (mg/DSCM) = 249.816
 DSCFM = 366,803 Y (METER) = 1.03

TIME PER READING	METER	TEMPERATURE INLET	TEMPERATURE OUTLET	ORIFICE	O2	CO2
5	428.581	103	103	0	15.3	3.5
5		104	104	0		
5		106	103	0		
5		106	104	0		
5		106	104	0	15.2	3.6
5		105	105	0		
5		104	105	0		
5		105	105	0		
5		106	105	0	15.3	3.5
5		106	106	0		
5		106	106	0		
5	429.368	106	106	0	15.2	3.5

TIME	VM	TM		OR	O2	CO2
60	0.787	105		0	15.3	3.5

EMISSIONS

DRY:
 PPM, NOX = 130.7 MNBTU/HR = 618.0
 LBS/HR = 343.34
 LBS/MNBTU = 0.556

GILBERT/COMMONWEALTH, INC.
TESTING SERVICES GROUP

FIELD MOISTURE DETERMINATION

CLIENT: PECO

W.O. NO.: 6314-000

TEST: M-22-1 DATE: 7/18/91 TIME: 1252

OPERATOR: ALBRIGHT

BAROMETRIC PRESSURE: 29.88

GAS METER

START: 429.438 FINAL: 445.487 NET: 16.049

Y FACTOR= 1.03

FLOW METER

AVE. ORIFICE DROP 1.92 AVE. TEMPERATURE: 113

MOISTURE

IMP 1	START:	150	FINAL:	150	NET:	0
IMP 2	START:	150	FINAL:	160	NET:	10
IMP 3	START:	0	FINAL:	0	NET:	0
GEL	START:	239	FINAL:	243	NET:	4

TOTAL COLLECTED MOISTURE: 14.0

TOTAL MOISTURE BY WEIGHT: 4.1 %

SAMPLE VOLUME(CMNSTD): 15.286

GILBERT/COMMONWEALTH, INC.
TESTING SERVICES GROUP

CO EMISSIONS

CLIENT: PHILADELPHIA ELECTRIC COMPANY

LOCATION: CROYDON STATION

UNIT 22

LAB RESULTS CO, PPM BAG SAMPLE	% CO2 IN STACK	CO, PPM CORRECTED FOR CO2	CO LBS/SEC	FLOW DSCFM	CO LBS/HR	MMBTU/HR	CO LBS/MMBTU
RUN 1 0.90	3.80	0.87	6.32E-08	382,376	1.45	642	0.00226
RUN 2 1.10	3.85	1.06	7.72E-08	368,184	1.71	632	0.00270
RUN 3 1.50	3.53	1.45	1.06E-07	366,960	2.33	618	0.00376

APPENDIX B

CALIBRATION DATA

Gilbert/Commonwealth Inc.
 Testing Services Group
 METER BOX CALIBRATION

DATE: 7/19/91 METER BOX NUMBER: 1385

BAROMETRIC PRESS. (PB) = 29.49 in. Hg CALIBRATED BY: ROLAND

Orifice Manometer Setting (delta H) In. H ₂ O	GAS VOLUME			TEMPERATURES			Time min.	Yi	delta H0i
	Wet	Dry	Wet	Dry Gas Meter					
	Test Meter (Wt) cu. ft.	Gas Meter (Dt) cu. ft.	Test Meter (Wt) deg. F	Inlet (Tin) deg. F	Outlet (Tdn) deg. F	Average (Td) deg. F			
0.5	5.000	5.060	77.5	98.5	95.5	96.5	11.05	1.00	1.63
1.0	5.000	5.113	77.5	99	97.5	93.3	9.17	1.00	1.94
1.5	10.000	10.290	77.5	104	99.5	95.0	15.53	1.00	2.09
2.0	10.000	10.323	77.5	100.5	92.5	100.5	13.90	1.00	2.05
3.0	10.000	10.601	77.5	111	94	102.5	11.17	1.00	2.13
4.0	10.000	10.520	77.5	113.5	95.5	104.5	9.00	0.99	2.19
							AVERAGE Yi	1.00	2.01

FORMULAS

$$Y_i = \frac{(Wt) (Pb) (Tdr+460)}{(Wt) (Pb) (49/13.6) (Tdr+460)}$$

$$\text{delta H0i} = \frac{0.323}{(Wt) (Wt)}$$

$$K_0 = Q_0 \frac{(Pb) (29)}{V_i (Tdn+460) (\text{delta H})}$$

$$Q_0 = \frac{(V_0) (Tdr+460)}{(T_0) (Tdr+460)}$$

Gilbert/Concominalth Inc.
 Testing Services Group
 METER BOX CALIBRATION

DATE: 7/8/91 METER BOX NUMBER: 1385
 BAROMETRIC PRESS. (Pb) = 29.39 in. Hg CALIBRATED BY: ROLAND

Orifice Manometer Setting (delta H) In. H2O	GAS VOLUME		Inlet Temp (Tin) deg. F	TEMPERATURES			Time min.	Y1	delta H01
	Inlet Temp (Tin) deg. F	Dry Gas Meter (Vd) cu. ft.		Outlet Temp (Tou) deg. F	Dry Gas Meter				
					Inlet (Tds) deg. F	Outlet (Tdu) deg. F			
0.5	5.000	4.313	74.5	83.5	77.5	83.5	12.18	1.03	1.82
1.0	5.000	5.005	74.5	90	80.5	83.3	8.53	1.02	1.78
1.5	10.000	10.034	74.5	107	84.5	95.8	14.58	1.03	1.82
2.0	10.000	10.160	74.5	115.5	89	102.3	13.13	1.03	2.00
3.0	12.500	12.735	74.5	120.5	93.5	107.0	13.41	1.03	2.09
4.0	10.000	10.401	74.5	120	96.5	108.3	9.38	1.01	2.04
AVERAGE Y1								1.03	1.95

FORMULAS

$$Y_1 = \frac{(V_d)(P_b)(T_d+460)}{(V_d)(P_b+(3/13.6))(T_d+460)}$$

$$\text{delta H01} = \frac{0.321}{(P_d)(P_u)}$$

$$P_u = \frac{1 - (P_b)(29)}{V_1 - (T_d+460)(\text{delta H}_0)}$$

$$P_d = \frac{(V_d)(T_d+460)}{(T_u+460)}$$

GILBERT ASSOCIATES, INC.
ENGINEERS AND CONSULTANTS
READING, PA.

CLIENT

PROJECT

FILING CODE

W.C.

PAGE

OF

ENGINEER

KOCCAND

DATE

10/30/92

REVIEWED BY

DATE

SYSTEM

CALCULATION FOR

Pot Meter-Thermocouple Calibration

Pot Meter #

1

Thermocouple Type

K

Ice Bath Temperature °F

29

Certified Mercury Bulb °F

32

Ambient Temperature °F

67

Certified Mercury Bulb °F

67

Boiling H₂O °F

210

Certified Mercury Bulb °F

209

Hot Synthetic Oil °F

350

Certified Mercury Bulb °F

350

Remarks:

FILING
CODE
3000

APPENDIX 9

SAMPLE CALCULATIONS

SAMPLE CALCULATIONS

Particulate Isokinetic Sampling

I. Calculations for stack volume and Isokinetic Ratio

Time	Dry Gas Meter Ft ³	Pitoc	Orifice	Dry Gas		Stack	Stack Temp °F
		Δ P, In. H ₂ O	Δ H, In. H ₂ O	In.	Out	Pressure In. H ₂ O	
T	VM	Δ P	PM	TMI	TMO	PST	TS

1. DN = Nozzle Diameter, inches

2. PB = Barometric Pressure, inches Hg

3. TT = Net Sampling Time, minutes

4. VM = VM final - VM initial = Sample Gas Volume, ft³

5. TM = Average Dry Gas Temperature at Meter, °F

$$TM = \frac{\text{Avg. TMI} + \text{Avg. TMO}}{2}$$

6. PM = Average Orifice Pressure Drop, inches H₂O

$$PM = \text{Avg. } \Delta H$$

7. Volume of dry gas sampled at standard conditions^a, DSCF

$$VM_{STD} = \frac{17.65 \times VM \times T \left(\frac{PB + PM}{13.6} \right)}{(TM + 460)}$$

8. VW = Total Water Collected = gm H₂O Salica gel + ml Imp. H₂O = ml

9. Volume of water vapor at standard conditions^b, SCF

$$VW_{gas} = 0.0671 \times VW = \text{SCF}$$

10. Percent moisture in stack gas

$$\% M = \frac{100 \times VW_{gas}}{VM_{STD} + VW_{gas}}$$

11. Mole fraction of dry gas

$$MD = \frac{100 - \%M}{100}$$

12. Molecular weight of dry stack gas

$$MWD = (\%CO_2 \times \frac{44}{100}) + (\%O_2 \times \frac{32}{100}) + \left[(\%CO + \%N_2) \times \frac{28}{100} \right]$$

12A. XEA = % Excess Air = $\frac{[(\% O_2) - 0.5 (\% CO)]}{0.266 (\% N_2) - [(\% O_2) + 0.5 (\% CO)]} \times 100$

13. Molecular weight of wet stack gas

$$MW = MWD \times MD + 18 (1 - MD)$$

14. AS = Stack Area, square inches

15. PS = Stack Pressure, inches Hg

$$PS = PB \pm \text{Avg. PST}$$

NOTE: PST in. Hg. = $\frac{\text{PST in. H}_2\text{O}}{13.6}$

16. TS = Average Stack Temperature, °F

$$TS = \text{Average TS}$$

17. SDE = Average $\sqrt{\text{Velocity Head } (\Delta P) \times (\text{Stack Temperature} + 460)}$
(Calculated each line)

$$SDE = \text{Avg } \sqrt{\Delta P \times (TS + 460)}$$

18. Stack gas velocity at stack conditions, fpm

$$VS = 5130 \times Cp \times \text{Avg}(SDE) \times \left[\frac{1}{PS \times MW} \right]^{1/2} = \text{FPM} \quad \text{Cp} = \text{pitot tube coefficient}$$

19. Stack gas volumetric flow rate at standard conditions^c, DSCFM

$$Q_s = \frac{0.123 \times VS \times AS \times MD \times PS}{(TS + 460)} = \text{DSCFM}$$

20. Stack gas volumetric flow rate at stack conditions, ACFM

$$Q_a = \frac{0.05667 \times QS \times (TS + 460)}{PS \times MD} = \text{ACFM}$$

21. Percent Inertial

$$\%I = \frac{1.032 \times (TS + 460) \times VMSTD}{VS \times TT \times PS \times MD \times (DN)^2}$$

NOTES: ^aDry standard cubic feet at 69°F, 29.92 in. Hg.

^bStandard conditions at 68°F, 29.92 in. Hg.

^cDry standard cubic feet per minute at 68°F, 29.92 in. Hg.

II. Calculations for grain loading and emission rates

22. Particulate, gr/DSCF

$$\text{gr/DSCF} = 0.0154 \times \frac{\text{MR}}{\text{VMSTD}}$$

23. Particulate at stack conditions, gr/ACF

$$\text{gr/ACF} = \frac{17.65 \text{ gr/DSCF} \times \text{PS} \times \text{MD}}{(\text{TS} + 460)}$$

24. Particulate, lb/hr conc. method

$$\text{lb/hr} = 0.00857 \times \text{gr/DSCF} \times \text{QS}$$

25. Particulate lb/hr area method = $0.132 \times \frac{\text{RMS Particulate} \times \text{AS}}{\left(\frac{\text{DN}^2}{4}\right) \times \text{TI}}$

26. Particulate, combustion

$$\frac{\text{lb/hr}}{10^6 \text{ BTU/hr}}$$

27. Particulate, process lb/ton

$$\text{lb/ton} = \frac{\text{lb/hr}}{\text{tons/hr}}$$

28. Particulate, lb/MMBTU, F-Factor Method =

Unadj O_2 =

$$\frac{0.0154 \times \text{MR} \times \text{F-Factor} \times 20.9}{7000 \times \text{VMSTD} \times (20.9 - \text{O}_2)}$$

Unadj CO_2 =

$$\frac{0.0154 \times \text{MR} \times \text{F-Factor} \times 100}{7000 \times \text{VMSTD} \times \text{CO}_2}$$

29. F-Factor, dscf/mmBtu

O_2 Format:

$$\text{F-Factor} = \frac{10^6 (3.64(\text{RH}) + 1.53(\text{RC}) + 0.57(\text{RS}) + 0.14(\text{RN}) - 0.46(\text{CO}_2))}{\text{GCV}}$$

CO_2 Format:

$$\frac{10^6 (0.321)(\text{RC})}{\text{GCV}}$$

CALCULATION FOR NO_x, LBS/MMBtu - EPA METHOD 7D

Lab results in µgm NO₂

$$\text{Concentration } \mu\text{g/DSCM} = \frac{10^{-3} \text{ mg } [\mu\text{gm NO}_2]}{\frac{(100)}{100-360_2} \text{ Vol. (Fe}^3\text{)} \times 2.832 \times 10^{-2} \frac{\text{m}^3}{\text{Fe}^3}} \times \frac{\text{mg}}{\text{m}^3}$$

$$\text{NO}_x \text{ (ppm)} = \frac{\frac{\text{mg}}{\text{m}^3}}{1.912 \frac{\text{mg}}{\text{m}^3} / \text{ppm}}$$

Handwritten notes:
 1.912 mg/m³ = 10 ppm
 1.912 mg/m³ = 10 ppm

$$\text{NO}_x \text{, Lbs/SCF} = \text{PPM} \times 1.196 \times 10^{-7}$$

$$\text{NO}_x \text{, Lbs/Hr} = \text{Lbs/SCF} \times \text{Stack Gas Volume (DSCFM)} \times 60$$

$$\text{NO}_x \text{, Lbs/MMBtu} = \frac{\text{Lbs/Hr}}{\text{MMBtu/Hr}}$$

CALCULATIONS FOR CO LBS/MMBTU

Lab results reported in PPM(CO)

CO concentration corrected for CO₂ absorption by KMnO₄ scrubbing solution

$$C = C_b (1-F)$$

C = CO Conc. Dry Basis, ppm

C_b = CO Conc. Lab Results, ppm

F = % CO₂ In Stack

CO, Lbs/scf = ppm X 7.3 X 10⁻⁸

CO, Lbs/hr = Lbs/scf X Stack Gas Volume (DSCFM) X 60

CO, Lbs/MMBtu = Lbs/hr $\frac{1}{\text{MMBtu/hr}}$

Handwritten notes:
1.9107 $\frac{100}{100}$ $\frac{100}{100}$ $\frac{100}{100}$
2.85 $\frac{100}{100}$
1.16 $\frac{100}{100}$
3.16 $\frac{100}{100}$

SAMPLE CALCULATIONS

COMBUSTION CALCULATION FOR FLUE GAS FLOW AND LBS/MMBTU
Run No.

Fuel Analysis _____ BTU/lb _____ Lbs/gal
 _____ %C _____ %H
 _____ %O₂ _____ %S
 _____ %Ash

Fuel Consumption _____ gallons/hr
 _____ gallons/hr x _____ lbs/gallons = _____ lbs/hr

1. Theoretical Air (T.A.) = $144 \times \frac{\%C}{88} + 24 \times \frac{(\%H_2 - O_2/8) + 3(\%S)}{100} = \frac{\text{lb air}}{10,000 \text{ Btu}}$

2. Unburned Fuel Loss (UFL) = $\frac{\% \text{ Ash} \times \% \text{ combustibles}}{100\% \text{ combustibles}} = \text{_____ \%}$

As the % ash is only a trace amount, the % combustibles in the ash and the UFL are assumed to be zero.

3. Fuel Burned = $[100(100\% - \% \text{ Ash}) \times \text{BTU/lb fuel}] - .007 \times \text{UFL} = \text{_____ lb/fuel/10,000 BTU}$

Flue Gas Characteristics

_____ °F Stack Temperature, Barometer _____ in Hg
 _____ % CO₂ _____ % CO
 _____ % O₂ _____ % N₂
 _____ Static Pressure (inches H₂O)
 _____ % Moisture

% Excess Air = $\frac{(\% O_2 - 0.5(\% CO))}{0.264 (\% N) - [(\% O_2) + 0.5 (\% CO)]} \times 100 = \text{_____}$

4. Dry air (D.A.) = $\frac{100 + \% \text{ E.A.}}{100} (\text{T.A.} - 0.8 (\text{UFL})) = \text{_____ lb dry air/10,000 BTU}$

5. H₂O in Air = D.A. x 0.013 lb H₂O/lb dry air = _____ lb/H₂O/10,000 BTU

6. Wet Gas Total = Eq.3 + Eq.4 + Eq.5 = _____ lb/10,000 BTU

7. Total Flue Gas = Eq.6 x $\frac{\text{BTU/lb fuel}}{10,000}$ = _____ lb gas/lb fuel

8. Density of Gas @ _____ °F = $\frac{\text{Molecular Wt. of Wet Gas} \times 528}{385.1 \times (T_s + 460)}$ = _____ $\frac{\text{lb}}{\text{Cu. Ft.}}$

Molecular weight of wet stack gas

MW = MWID x MD + 18 (1-MD)

Mole fraction of dry gas

MD = $\frac{100 - \%M}{100}$

Molecular weight of dry stack gas

MWID = $\frac{(\%CO_2 \times 44)}{100} + \frac{(\%O_2 \times 32)}{100} + \frac{(\%CO + \%N_2) \times 28}{100}$

9. Total Flue Gas Flow = Eq.7 x lbs fuel/hr x $\frac{\text{hour}}{60 \text{ minutes}}$ x $\frac{1}{\text{Eq. 8}}$ = _____ ACFM

10. Qs(dscfm) = $\frac{Qa(acfm) \times Md \times Ps}{0.05645 \times (T_s + 460)}$ = _____ dscfm

PS = $\frac{\text{Barometric Pressure} + \text{Static Pressure}}{13.6}$

11. NO_x (lbs/hr) = NO_x (ppm) x 1.194 x 10⁻⁷ x DSCFM x 60 = lbs/hr NO_x

12. NO_x(lbs.) = $\frac{\text{lbs./hour}}{\text{MMBtu}}$

MMBtu/hr = Fuel Consumption lbs/hr x Btu/lb

MMBtu/hr = _____ x _____ = _____