

AMOCO PRODUCTION COMPANY

MORGANZA FIELD CTB #1 AND SWEETENING FACILITY

MORGANZA, (POINTE COUPEE PARISH) LOUISIANA

OXIDES OF NITROGEN, CARBON MONOXIDE  
and OPACITY

SOURCE # 87-4

JUNE 28, 1988

Submitted By :

EMISSION TESTING SERVICES, INC.

POST OFFICE BOX 15075

BATON ROUGE, LOUISIANA 70895

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AIR QUALITY DIVISION

**EMISSION TESTING SERVICES, INC.**

**POST OFFICE BOX 15075**

**BATON ROUGE, LOUISIANA 70895**

**CONFIRMATION OF INFORMATION**

**EMISSION TEST REPORT**

**FOR**

**AMOCO PRODUCTION COMPANY**

**MORGANZA CTB # 1 AND SWEETENING FACILITY**

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**OXIDES OF NITROGEN, CARBON MONOXIDE  
and OPACITY**

**SOURCE # 87-4**

**JUNE 28, 1988**

I certify that I have personally examined and am familiar with the information submitted herein, and based on my inquiries of those individuals immediately responsible for obtaining the information, I believe the submitted information is true, accurate, and complete.

\_\_\_\_\_  
J. ANGELLOZ  
Project Leader

\_\_\_\_\_  
Barry Gipson  
Manager

OXIDES OF NITROGEN, CARBON MONOXIDE  
and OPACITY

EMISSIONS TESTING

SOURCE # 87-4

for

AMOCO PRODUCTION COMPANY

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## I. INTRODUCTION

Emission Testing Services, Inc. was contracted by AMOCO Production Company to perform emissions testing on cogeneration Turbine 87-4 located at Morganza, Louisiana. This turbine is addressed in DEQ air permit No. 2260-00025-00. Testing was conducted for oxides of nitrogen, carbon monoxide emissions and opacity of emissions.

Turbine unit 87-4 consists of a natural gas fired turbine, an 800 kw/hour electric generator and a thermo flood heat recovery system. The turbine was manufactured by Solar turbines, Inc., model GCI-SB-KATO, serial no. SG87917.

Emissions were determined using EPA Method 9 for visible emissions, EPA Method 10 for carbon monoxide emissions, and EPA Method 20, as modified by Subpart GG, for Oxides of nitrogen emissions. The number of traverse points and the stack gas moisture, velocity and dry molecular weight were determined using EPA Methods 1-4. EPA Methods are found in Appendix A, Part 60, Title 40 of the Code of Federal Regulations.

The testing team consisting of John Angeloz, Troy LeSage, and Steven Schwartz arrived on June 27, 1988. All equipment was set-up and the instrumentation checked out. Testing began on the 28th with Steven Schwartz responsible for testing of oxides of nitrogen and carbon monoxide. John Angeloz was responsible for determining stack gas velocity, volumetric flow and opacity of emissions.

Three test runs were completed on the unit at maximum load conditions. During each test run, AMOCO personnel collected fuel gas samples for analysis and recorded turbine operational data. This analytical and operating data is included in the appendix.

Testing was coordinated through J.G. Lemaire of Amoco.

II. **SUMMARY**

Emission testing results from Turbine 87-4 are tabulated below. Stack gas flow data follow on the next page.

Oxides of nitrogen (NOX) results have been reported as nitrogen dioxide. NOX emission rate data have been corrected to ISO standard day conditions. Concentration data reported as parts per million (PPM) have been corrected to 15 percent oxygen and ISO standard day conditions as outlined in Subpart GG of the regulations.

TURBINE 87-4

JUNE 28, 1988

<u>PARAMETER</u>	<u>RUN 1</u>	<u>RUN 2</u>	<u>RUN 3</u>	<u>AVG.</u>
TIME	0845-0945	1100-1200	1300-1400	
OXIDES OF NITROGEN ( PPM )	52.416	52.856	49.124	51.465
( lb/ Hr )	2.576	2.491	2.468	2.512
CARBON MONOXIDE ( lb/ Hr )	1.987	1.932	1.960	1.960
OPACITY ( % )				
maximum	0	0	0	0
minimum	0	0	0	0
average	0	0	0	0
FUEL FEED RATE (MCFD)	279	260	260	266
GENERATOR LOAD (kw)	778	745	746	756

TURBINE 87-4

JUNE 28, 1988

RUN NO.	PHYSICAL DATA ON STACK GAS			
	TEMPERATURE DEG. R	MOISTURE %	VELOCITY ft/ sec	VOLUMETRIC FLOW DSCFM
1	1258	7.29	137.51	10112
2	1276	7.35	137.05	9945
3	1265	5.98	135.81	10084
AVG.	1266	6.87	136.79	10047

### III. PROCEDURE

Reference Methods 1 - 4 were followed to establish traverse points, stack gas velocity, dry gas molecular weight and moisture content of the gas stream. Method 20 was used to determine oxides of nitrogen concentration, Method 10 was used to determine carbon monoxide concentration and Method 9 was used to determine visible emissions. A brief description of each method used follows.

#### METHOD 1: SAMPLE AND VELOCITY TRAVERSES FOR STATIONARY SOURCES

Sampling and velocity measurements were performed at a point meeting the "8 and 2" requirement.

#### METHOD 2: DETERMINATION OF STACK GAS VELOCITY AND VOLUMETRIC FLOW RATE (TYPE S PITOT TUBE)

The average gas velocity in the stack was determined from the gas molecular weight, moisture content and the measurement of the average velocity head with a type "S" pitot tube. Dry volumetric flow rate was determined from the velocity and stack diameter.

#### METHOD 3: GAS ANALYSIS FOR CARBON DIOXIDE, OXYGEN, EXCESS AIR, AND DRY MOLECULAR WEIGHT

The dry molecular weight of the stack gas was determined using an Orsat analyzer. The Orsat measures the concentration of oxygen, carbon monoxide and carbon dioxide. The remaining gas components are assumed to be nitrogen.

#### METHOD 4: DETERMINATION OF MOISTURE CONTENT IN STACK GASES

A gas sample was extracted from the stack using a heated glass probe fitted with a particulate filter. The sample gas then passed through a series of four impingers immersed in an ice bath. The first two impingers contained measured volumes of water, the third was empty, and the fourth contained a known weight of silica gel. Any water vapor in the gas stream was condensed and trapped in the impingers. Moisture was determined gravimetrically.



**METHOD 9: VISUAL DETERMINATION OF THE OPACITY OF EMISSIONS FROM STATIONARY SOURCES**

Emissions opacity is determined visually by a certified observer. The method specifies procedures for observation of the visible plume emitted from the stack.

**METHOD 10: DETERMINATION OF CARBON MONOXIDE EMISSIONS FROM STATIONARY SOURCES**

An continuous gas sample was extracted from the stack at a centroidal sampling point. The sample was transferred through a heated sample line to a carbon dioxide scrubber and then to a Luft-type nondispersive infrared analyzer (NDIR) for analysis of carbon monoxide.

**METHOD 20: DETERMINATION OF NITROGEN OXIDES, SULFUR DIOXIDE, AND OXYGEN EMISSIONS FROM STATIONARY GAS FIRED TURBINES**

A continuous gas sample was extracted from the stack at a centroidal sampling point. The sample was transferred through a heated sample line to a chemiluminescence analyzer for analysis of nitrogen oxides concentration.

**IV. ANALYTICAL TECHNIQUE**

All samples collected were analyzed in the field using continuous analyzers. Oxides of nitrogen concentration was determined using a chemiluminescence analyzer and carbon monoxide concentration was determined using a nondispersive infrared analyzer.

V. **CHAIN of CUSTODY**

No samples were transported to the laboratory for analysis.

VI. **TEST DATA & CALCULATIONS**

All data obtained during testing are contained in this section along with the associated data reduction calculations. Turbine operating data collected during testing and fuel gas analysis are also included at the end of this section.

## Traverse Point Layout

Client Amoco

Date 06-27-88

Unit Tested Turbine

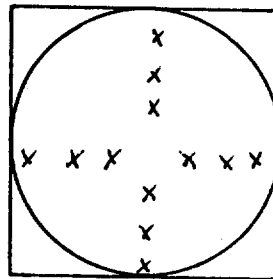
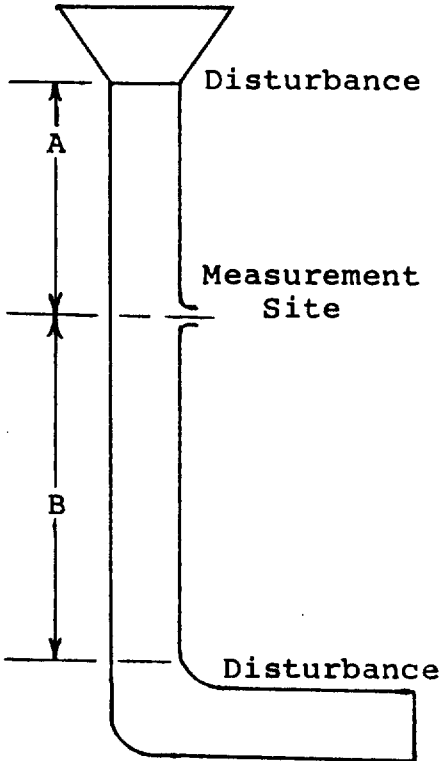
Location Morganza, LA.

Upstream Distance (A) \_\_\_\_\_

Downstream Distance (B) \_\_\_\_\_

Inside Diameter 24"

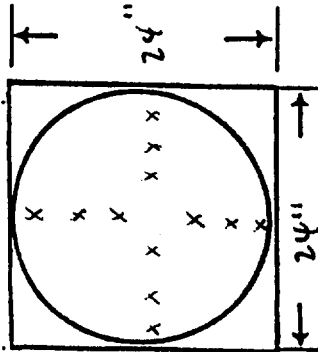
Coupling Length 8.5"



Cross Section Schematic of Stack

Traverse Point	Distance % of Diameter	Stack Diameter	Coupling Length	Traverse Points
1	<u>.044</u>	<u>24"</u>	<u>8.5"</u>	<u>9.556</u>
2	<u>.146</u>	<u>"</u>	<u>"</u>	<u>12.004</u>
3	<u>.296</u>	<u>"</u>	<u>"</u>	<u>15.604</u>
4	<u>.704</u>	<u>"</u>	<u>"</u>	<u>25.396</u>
5	<u>.854</u>	<u>"</u>	<u>"</u>	<u>28.996</u>
6	<u>.956</u>	<u>"</u>	<u>"</u>	<u>31.444</u>
7	_____	_____	_____	_____
8	_____	_____	_____	_____
9	_____	_____	_____	_____
10	_____	_____	_____	_____
11	_____	_____	_____	_____

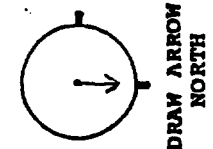
CROSS SECTIONAL SCHEMATIC OF STACK  
TRAVERSE POINT LAYOUT



ETS

FIELD DATA, METHOD(S)

1-4



PLANT Amoco STACK DIAMETER, in. 24"  
 DATE 06-28-88 PITOT TUBE NO. P-3-3  
 LOCATION Morganza La. AMBIENT TEMPERATURE 85°F  
 OPERATOR K. Thibodeaux BAROMETRIC PRESSURE 29.96  
 STACK NO. Turbine FILTER TAPE wt mg —  
 RUN NO. 1 PROBE LENGTH, in. 3'  
 SAMPLE BOX NO. 00 METER BOX NO. 586  
 METER BOX NO. 586 PITOT FACTOR 1.800  
 AMBIENT TEMPERATURE 85°F METER Δ Hg 1.844  
 BAROMETRIC PRESSURE 29.96 D.G.M.C. FACTOR 1.037  
 FILTER TAPE wt mg — K FACTOR —  
 PROBE LENGTH, in. 3'

TRAVERSE POINT NUMBER	SAMPLING TIME (t), min.	STATIC PRESSURE (in. H <sub>2</sub> O)	STACK TEMP (t <sub>s</sub> ), °F	VELOCITY HEAD (ΔP) <sub>s</sub> (1/ΔP) <sub>s</sub>	PRESSURE DIFFERENTIAL ACROSS ORIFICE METER in. H <sub>2</sub> O		GAS SAMPLE VOLUME (V <sub>m</sub> ), lb	GAS SAMPLE TEMPERATURE AT DRY GAS METER		SAMPLE BOX TEMPERATURE °F	TEMPERATURE OF GAS LEAVING CONDENSER OR LAST IMPINGER °F	PUMP VACUUM in. Hg gauge
					ACTUAL DESIRED	in. H <sub>2</sub> O		INLET (T <sub>min</sub> ), °F	OUTLET (T <sub>max</sub> ), °F			
1	0845	0.605	723	2.250	1.500	1.500	180.501	77	81	226	63	7.0
2	0850	off	776	2.400	1.550	1.550	186.441	82	89	242	65	6.9
3	0900	off	808	2.700	1.643	1.500	201.643					
4	0923	off	813	3.000	1.732							
5			808	3.100	1.760							
6			814	3.050	1.746							
7			791	2.150	1.470							
8			804	2.650	1.630							
9			812	3.000	1.732							
10			811	2.850	1.690							
11			809	3.100	1.760							
12			811	2.550	1.600							
AVERAGE	28	0.605	798		1.651	1.5	21.142					

82

COMMENTS:

PRE-LEAK CHECK GOOD @ 9.9" H.G.  
 POST-LEAK CHECK GOOD @ 8.0" H.G.  
 Pitot Tube Leak Check  
 Good @ 6.1" H<sub>2</sub>O  
 Det-89°F

ORSAT MEASUREMENT

	CO <sub>2</sub>	O <sub>2</sub>	CO	N <sub>2</sub>
1	2.4	16.9	0.0	80.7
2				
3				
4				

IMPINGER WEIGHTS

VOLUME OF LIQUID WATER COLLECTED	FINAL	INITIAL	WEIGHT COLLECTED	TOTAL WEIGHT
	559.8	558.1	448.3	569.7
	537.7	552.2	448.3	562.3
	22.1	5.7	0.4	7.2
				35.6

Emission Testing Services, Inc.  
 P.O. Box 15075  
 Baton Rouge, LA 70895  
 504-925-8405

Client : AMOCO  
 Source : TURBINE  
 Testing Date : 6-28-88  
 Run : 1

DETERMINATION OF STACK GAS MOISTURE CONTENT

- Bws - Moisture fraction content
- Mw - Molecular weight of water, 18.0 lb/ lb mole
- Pm - Absolute pressure at meter, in-Hg
- Ps - Standard absolute pressure, 29.92 in-Hg
- R - Ideal gas constant, 21.85 in-Hg ft<sup>3</sup>/ lb-mole deg R
- Tm - Absolute temperature at meter, deg R
- Ts - Standard absolute temperature, 528 deg R
- Vm - Dry gas volume measured by meter, DCF
- Vms - Dry gas volume at standard conditions, DSCF
- Vwc - Volume of water vapor collected by impingers, SCF
- Vwsg - Volume of water vapor collected by silica gel, SCF
- Wc - Total weight of impinger water, lb
- Wsg - Total weight of silica gel water, lb
- Y - Dry gas meter calibration factor

$$Wc = ( 22.1 \text{ g}) + ( 5.9 \text{ g}) + ( .4 \text{ g}) / (453.6 \text{ g/lb}) = .06261$$

$$Wsg = ( 7.2 \text{ g}) / (453.6 \text{ g/lb}) = .01587$$

$$Vwc = \frac{Wc R Ts}{Ps Mw} = \frac{( .06261 ) ( 21.85 ) ( 528 )}{( 29.92 ) ( 18.0 )} = 1.34121$$

$$Vwsg = \frac{Wsg R Ts}{Ps Mw} = \frac{( .01587 ) ( 21.85 ) ( 528 )}{( 29.92 ) ( 18.0 )} = .34003$$

$$Vms = Vm Y \frac{Pm Ts}{Ps Tm} = ( 21.142 ) ( 1.037 ) \frac{( 29.96 ) ( 528 )}{( 29.92 ) ( 542. )} = 21.37663$$

$$Bws = \frac{Vwc + Vwsg}{Vwc + Vwsg + Vms} = \frac{( 1.34121 ) + ( .34003 )}{( 1.34121 ) + ( .34003 ) + ( 21.37663 )} = .0729$$

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504-925-8405

Client : AMOCO  
Source : TURBINE  
Testing Date : 6-28-88  
Run : 1

DETERMINATION OF DRY MOLECULAR WEIGHT

Md - Dry molecular weight, lb/ lb-mole  
%CO2 - Percent CO2 by volume ( dry basis )  
%O2 - Percent O2 by volume ( dry basis )  
%CO - Percent CO by volume ( dry basis )  
%N2 - Percent N2 by volume ( dry basis )  
0.280 - Molecular weight of N2 or CO, divided by 100  
0.320 - Molecular weight of O2, divided by 100  
0.440 - Molecular weight of CO2, divided by 100

$$Md = 0.440( \%CO_2 ) + 0.320( \%O_2 ) + 0.280( \%N_2 + \%CO )$$

$$Md = 0.440( 2.4 ) + 0.320( 16.9 ) + 0.280( 80.7 + .0 )$$
$$= 29.060$$

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P.O. Box 15075  
Baton Rouge, LA 70895  
504-925-8405

Client : AMOCO  
Source : TURBINE  
Testing Date : 6-28-88  
Run : 1

DETERMINATION OF STACK GAS VELOCITY AND VOLUMETRIC FLOW RATE

- A - Cross-sectional area of stack, ft<sup>2</sup>
- Bws - Moisture fraction of stack gas
- Cp - Pitot tube coefficient
- dP - Average, square root of velocity head of stack gas
- Kp - Pitot tube constant,  
ft/sec ( lb in-Hg/ lb-mole deg R in Hg)<sup>0.5</sup>
- Md - Molecular weight of stack gas, dry basis, lb/ lb-mole
- Ms - Molecular weight of stack gas, wet basis, lb/ lb-mole
- Pbar - Barometric pressure at measurement site, in-Hg
- Pg - Static pressure of the stack gas, in H<sub>2</sub>O
- Ps - Absolute stack gas pressure, in-Hg
- Pstd - Standard absolute pressure, 29.92 in-Hg
- Qsd - Dry volumetric stack gas flow rate  
standard conditions, DSCF/Hr
- Ts - Average stack gas temperature, deg R
- Tstd - Standard absolute temperature, 528 deg R
- Vs - Average stack gas velocity, ft/sec
- 3600 - Conversion factor, sec to Hr
- 18.0 - Molecular weight of water, lb/lb-mole

$$Ms = Md ( 1 - Bws ) + 18.0 ( Bws ) =$$

$$= ( 29.060 ) ( 1 - .0729 ) + ( 18.0 ) ( .0729 ) = 28.254$$

$$Vs = Kp Cp Dp \left( \frac{Ts}{Ps Ms} \right)^{0.5} =$$

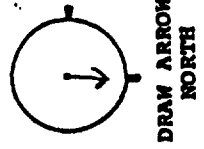
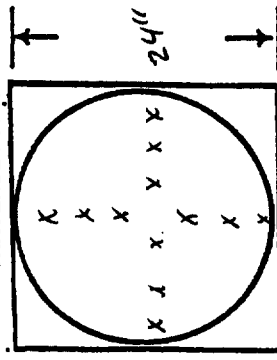
$$= ( 85.49 ) ( .800 ) ( 1.650 ) \left( \frac{1258.}{[ 30.004 ][ 28.254 ]} \right)^{0.5} = 137.5098$$

$$Qsd = 3600 ( 1 - Bws ) Vs A \frac{Tstd}{Ts} \frac{Ps}{Pstd} =$$

$$Qsd = 3600 ( 1 - .0729 ) ( 137.5098 ) ( 3.1416 ) \frac{( 528 ) ( 30.004 )}{( 1258. ) ( 29.92 )}$$

$$= 606692.7$$

CROSS SECTIONAL SCHEMATIC OF STACK  
TRAVERSE POINT LAYOUT



ETS FIELD DATA, METHOD(S) 1-4

PLANT Ardee SAMPLE BOX NO. EE STACK DIAMETER, in. 24"  
 DATE 062888 METER BOX NO. 586 PITOT TUBE NO. P-3-3  
 LOCATION Morganza Ch. AMBIENT TEMPERATURE 92.0F PITOT FACTOR 1.800  
 OPERATOR K. Thibodeaux BAROMETRIC PRESSURE 29.97 METER Δ Hg 1.844  
 STACK NO. Turbine FILTER TARE wt mg - D.G.M.C. FACTOR 1.037  
 RUN NO. 2 PROBE LENGTH, in. 3' K FACTOR -

TRAVERSE POINT NUMBER	SAMPLING TIME (9% min.)	STATIC PRESSURE (in. H <sub>2</sub> O)	STACK TEMP (1%), °F	VELOCITY HEAD (ΔP) (1/ΔP)	PRESSURE DIFFERENTIAL ACROSS ORIFICE METER (ΔH) in. H <sub>2</sub> O	GAS SAMPLE VOLUME (V <sub>m</sub> ), l/s	GAS SAMPLE TEMPERATURE AT DRY GAS METER		SAMPLE BOX TEMPERATURE °F	TEMPERATURE OF GAS LEAVING CONDENSER OR LAST IMPINGER °F	PUMP VACUUM in. Hg gauge
							INLET (T <sub>meas</sub> ), °F	OUTLET (T <sub>meas</sub> ), °F			
1	1100	10.650	793	2.150	1.500	202.047	97	100	242	66	2.0
2	1137	off	804	2.200	1.500	223.102	103	110	276	58	2.0
3			808	2.550	1.500						
4			817	3.100	1.500						
5			818	2.550	1.500						
6			823	3.050	1.746						
7			803	2.950	1.718						
8			818	2.650	1.628						
9			826	2.700	1.643						
10			827	2.700	1.643						
11			825	2.600	1.612						
12			826	2.750	1.718						
AVERAGE	32 min	10.650	815.66	1.635	1.500	21.055		102.5			

COMMENTS:

Dry - 103°F  
 PRE-LEAK CHECK GOOD @ 11" H.G.  
 POST-LEAK CHECK GOOD @ Wet - 88°F

VOLUME OF LIQUID WATER COLLECTED	IMPINGER WEIGHTS			
	FINAL	INITIAL	WEIGHT COLLECTED	TOTAL WEIGHT
	545.4	547.1	438.9	554.4
	542.4	541.2	432.0	545.7
	18.0	5.9	1.9	81.7
				345

	ORSAT MEASUREMENT			
	CO <sub>2</sub>	O <sub>2</sub>	CO	N <sub>2</sub>
1	2.4	17.0	0.0	80.6
2				
3				
4				

Pitot tube Check Good 4.5" H<sub>2</sub>O



Emission Testing Services, Inc.  
 P.O. Box 15075  
 Baton Rouge, LA 70895  
 504-925-8405

Client : AMOCO  
 Source : TURBINE  
 Testing Date : 6-28-88  
 Run : 2

DETERMINATION OF STACK GAS MOISTURE CONTENT

- Bws - Moisture fraction content
- Mw - Molecular weight of water, 18.0 lb/ lb mole
- Pm - Absolute pressure at meter, in-Hg
- Ps - Standard absolute pressure, 29.92 in-Hg
- R - Ideal gas constant, 21.85 in-Hg ft<sup>3</sup>/ lb-mole deg R
- Tm - Absolute temperature at meter, deg R
- Ts - Standard absolute temperature, 528 deg R
- Vm - Dry gas volume measured by meter, DCF
- Vms - Dry gas volume at standard conditions, DSCF
- Vwc - Volume of water vapor collected by impingers, SCF
- Vwsg - Volume of water vapor collected by silica gel, SCF
- Wc - Total weight of impinger water, lb
- Wsg - Total weight of silica gel water, lb
- Y - Dry gas meter calibration factor

$$Wc = ( 18.0 \text{ g}) + ( 5.9 \text{ g}) + ( 1.9 \text{ g}) / (453.6 \text{ g/lb}) = .05688$$

$$Wsg = ( 8.7 \text{ g}) / (453.6 \text{ g/lb}) = .01918$$

$$Vwc = \frac{Wc R Ts}{Ps Mw} = \frac{( .05688 ) ( 21.85 ) ( 528 )}{( 29.92 ) ( 18.0 )} = 1.21842$$

$$Vwsg = \frac{Wsg R Ts}{Ps Mw} = \frac{( .01918 ) ( 21.85 ) ( 528 )}{( 29.92 ) ( 18.0 )} = .41086$$

$$Vms = Vm Y \frac{Ps Ts}{Pm Tm} = ( 21.055 ) ( 1.037 ) \frac{( 29.92 ) ( 528 )}{( 29.92 ) ( 563. )} = 20.54284$$

$$Bws = \frac{Vwc + Vwsg}{Vwc + Vwsg + Vms} = \frac{( 1.21842 ) + ( .41086 )}{( 1.21842 ) + ( .41086 ) + ( 20.54284 )} = .0735$$

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504-925-8405

Client : AMOCO  
Source : TURBINE  
Testing Date : 6-28-88  
Run : 2

DETERMINATION OF DRY MOLECULAR WEIGHT

Md - Dry molecular weight, lb/ lb-mole  
%CO2 - Percent CO2 by volume ( dry basis )  
%O2 - Percent O2 by volume ( dry basis )  
%CO - Percent CO by volume ( dry basis )  
%N2 - Percent N2 by volume ( dry basis )  
0.280 - Molecular weight of N2 or CO, divided by 100  
0.320 - Molecular weight of O2, divided by 100  
0.440 - Molecular weight of CO2, divided by 100

$$M_d = 0.440( \%CO_2 ) + 0.320( \%O_2 ) + 0.280( \%N_2 + \%CO )$$

$$M_d = 0.440( 2.4 ) + 0.320( 17.0 ) + 0.280( 80.6 + .0 )$$

$$= 29.064$$

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Client : AMOCO  
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Testing Date : 6-28-88  
Run : 2

DETERMINATION OF STACK GAS VELOCITY AND VOLUMETRIC FLOW RATE

- A - Cross-sectional area of stack, ft<sup>2</sup>
- Bws - Moisture fraction of stack gas
- Cp - Pitot tube coefficient
- dP - Average, square root of velocity head of stack gas
- Kp - Pitot tube constant,  
ft/sec ( lb in-Hg/ lb-mole deg R in Hg)<sup>0.5</sup>
- Md - Molecular weight of stack gas, dry basis, lb/ lb-mole
- Ms - Molecular weight of stack gas, wet basis, lb/ lb-mole
- Pbar - Barometric pressure at measurement site, in-Hg
- Pg - Static pressure of the stack gas, in H<sub>2</sub>O
- Ps - Absolute stack gas pressure, in-Hg
- Pstd - Standard absolute pressure, 29.92 in-Hg
- Qsd - Dry volumetric stack gas flow rate  
standard conditions, DSCF/Hr
- Ts - Average stack gas temperature, deg R
- Tstd - Standard absolute temperature, 528 deg R
- Vs - Average stack gas velocity, ft/sec
- 3600 - Conversion factor, sec to Hr
- 18.0 - Molecular weight of water, lb/lb-mole

$$Ms = Md ( 1 - Bws ) + 18.0 ( Bws ) =$$

$$= ( 29.064 ) ( 1 - .0735 ) + ( 18.0 ) ( .0735 ) = 28.251$$

$$Vs = Kp Cp Dp \left( \frac{Ts}{Ps Ms} \right)^{0.5} =$$

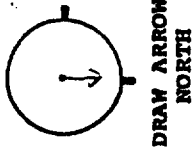
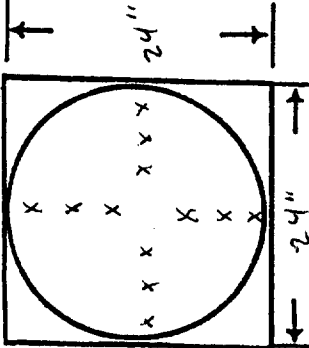
$$= ( 85.49 ) ( .800 ) ( 1.634 ) \left( \frac{1276.}{[ 30.038 ][ 28.251 ]} \right)^{0.5} = 137.0463$$

$$Qsd = 3600 ( 1 - Bws ) Vs A \frac{Tstd}{Ts} \frac{Ps}{Pstd} =$$

$$Qsd = 3600 ( 1 - .0735 ) ( 137.0463 ) ( 3.1416 ) \frac{( 528 ) ( 30.038 )}{( 1276. ) ( 29.92 )}$$

$$= 596727.0$$

CROSS SECTIONAL SCHEMATIC OF STACK  
TRAVERSE POINT LAYOUT



# ETS FIELD DATA, METHOD(S)

1-4

PLANT Amoco SAMPLE BOX NO. 00 STACK DIAMETER, in. 24"  
 DATE 0628-88 METER BOX NO. 586 PITOT TUBE NO. P-3-3  
 LOCATION Madagascar AMBIENT TEMPERATURE 98°F PITOT FACTOR 1.800  
 OPERATOR K. Thibodeaux BAROMETRIC PRESSURE 29.98 METER Δ Hg 1.844  
 STACK NO. Turbine FILTER TARE wt mg — D.G.M.C. FACTOR 1.037  
 RUN NO. 3 PROBE LENGTH, in. 3' K FACTOR —

TRAVERSE POINT NUMBER	SAMPLING TIME (Ø), min.	STATIC PRESSURE (in. H <sub>2</sub> O)	STACK TEMP (T <sub>s</sub> ), °F	VELOCITY HEAD (ΔP <sub>v</sub> ) (1/ΔP <sub>v</sub> )	PRESSURE DIFFERENTIAL ACROSS ORIFICE METER (ΔH) in. H <sub>2</sub> O ACTUAL DESIRED	GAS SAMPLE VOLUME (V <sub>m</sub> ), ft <sup>3</sup>	GAS SAMPLE TEMPERATURE AT DRY GAS METER		SAMPLE BOX TEMPERATURE °F	TEMPERATURE OF GAS LEAVING CONDENSER OR LAST IMPINGER °F	PUMP VACUUM in. Hg gauge
							INLET (T <sub>in</sub> ), °F	OUTLET (T <sub>out</sub> ), °F			
1	1307	70.650	677	1.850	1.500	223.259	113	115	250	62	6.2
2	1339	70.650	805	2.200	1.500	244.444	110	116	246	60	6.5
3			821	2.800	1.500						
4			829	3.150	1.500						
5			811	2.550	1.500						
6			819	3.050	1.500						
7			799	2.500	1.500						
8			814	2.700	1.500						
9			816	2.700	1.500						
10			827	2.800	1.500						
11			826	3.050	1.500						
12			817	2.700	1.500						
AVERAGE	32 min	70.650	804.7	1.636	1.500	21.185					

COMMENTS:

Wet - 86°F

PRE-LEAK CHECK GOOD @ 10.1" H.G.

POST-LEAK CHECK GOOD @ 7.1" H.G.

Pitot tube check Good @ 7.2" H<sub>2</sub>O

	ORSAT MEASUREMENT			
	CO <sub>2</sub>	O <sub>2</sub>	CO	N <sub>2</sub>
1	7.4	16.8	0.0	80.8
2				
3				
4				

VOLUME OF LIQUID WATER COLLECTED	IMPINGER WEIGHTS	
	INITIAL	FINAL
WEIGHT COLLECTED	24.1	2.3
TOTAL WEIGHT		21.3

Emission Testing Services, Inc.  
P.O. Box 15075  
Baton Rouge, LA 70895  
504-925-8405

Client : AMOCO  
Source : TURBINE  
Testing Date : 6-28-88  
Run : 3

DETERMINATION OF STACK GAS MOISTURE CONTENT

- Bws - Moisture fraction content
- Mw - Molecular weight of water, 18.0 lb/ lb mole
- Pm - Absolute pressure at meter, in-Hg
- Ps - Standard absolute pressure, 29.92 in-Hg
- R - Ideal gas constant, 21.85 in-Hg ft<sup>3</sup>/ lb-mole deg R
- Tm - Absolute temperature at meter, deg R
- Ts - Standard absolute temperature, 528 deg R
- Vm - Dry gas volume measured by meter, DCF
- Vms - Dry gas volume at standard conditions, DSCF
- Vwc - Volume of water vapor collected by impingers, SCF
- Vwsg - Volume of water vapor collected by silica gel, SCF
- Wc - Total weight of impinger water, lb
- Wsg - Total weight of silica gel water, lb
- Y - Dry gas meter calibration factor

$$Wc = ( 24.1 \text{ g}) + ( 2.3 \text{ g}) + ( .2 \text{ g}) / (453.6 \text{ g/lb}) = .05864$$

$$Wsg = ( .7 \text{ g}) / (453.6 \text{ g/lb}) = .00154$$

$$Vwc = \frac{Wc R Ts}{Ps Mw} = \frac{( .05864 )( 21.85 )( 528 )}{( 29.92 )( 18.0 )} = 1.25621$$

$$Vwsg = \frac{Wsg R Ts}{Ps Mw} = \frac{( .00154 )( 21.85 )( 528 )}{( 29.92 )( 18.0 )} = .03306$$

$$Vms = Vm Y \frac{Pm Ts}{Ps Tm} = ( 21.185 )( 1.037 ) \frac{( 29.98 )( 528 )}{( 29.92 )( 574. )} = 20.26645$$

$$Bws = \frac{Vwc + Vwsg}{Vwc + Vwsg + Vms} = \frac{( 1.25621 ) + ( .03306 )}{( 1.25621 ) + ( .03306 ) + ( 20.26645 )} = .0598$$

Emission Testing Services, Inc.  
P.O. Box 15075  
Baton Rouge, LA 70895  
504-925-8405

Client : AMOCO  
Source : TURBINE  
Testing Date : 6-28-88  
Run : 3

DETERMINATION OF DRY MOLECULAR WEIGHT

Md - Dry molecular weight, lb/ lb-mole  
%CO2 - Percent CO2 by volume ( dry basis )  
%O2 - Percent O2 by volume ( dry basis )  
%CO - Percent CO by volume ( dry basis )  
%N2 - Percent N2 by volume ( dry basis )  
0.280 - Molecular weight of N2 or CO, divided by 100  
0.320 - Molecular weight of O2, divided by 100  
0.440 - Molecular weight of CO2, divided by 100

$$Md = 0.440( \%CO2 ) + 0.320( \%O2 ) + 0.280( \%N2 + \%CO )$$

$$Md = 0.440( 2.4 ) + 0.320( 16.8 ) + 0.280( 80.8 + .0 )$$
$$= 29.056$$

Emission Testing Services, Inc.  
 P.O. Box 15075  
 Baton Rouge, LA 70895  
 504-925-8405

Client : AMOCO  
 Source : TURBINE  
 Testing Date : 6-28-88  
 Run : 3

DETERMINATION OF STACK GAS VELOCITY AND VOLUMETRIC FLOW RATE

- A - Cross-sectional area of stack, ft<sup>2</sup>
- Bws - Moisture fraction of stack gas
- Cp - Pitot tube coefficient
- dP - Average, square root of velocity head of stack gas
- Kp - Pitot tube constant, ft/sec ( lb in-Hg/ lb-mole deg R in Hg)<sup>1/2</sup>0.5
- Md - Molecular weight of stack gas, dry basis, lb/ lb-mole
- Ms - Molecular weight of stack gas, wet basis, lb/ lb-mole
- Pbar - Barometric pressure at measurement site, in-Hg
- Pg - Static pressure of the stack gas, in H<sub>2</sub>O
- Ps - Absolute stack gas pressure, in-Hg
- Pstd - Standard absolute pressure, 29.92 in-Hg
- Qsd - Dry volumetric stack gas flow rate standard conditions, DSCF/Hr
- Ts - Average stack gas temperature, deg R
- Tstd - Standard absolute temperature, 528 deg R
- Vs - Average stack gas velocity, ft/sec
- 3600 - Conversion factor, sec to Hr
- 18.0 - Molecular weight of water, lb/lb-mole

$$Ms = Md ( 1 - Bws ) + 18.0 ( Bws ) =$$

$$= ( 29.056 ) ( 1 - .0598 ) + ( 18.0 ) ( .0598 ) = 28.395$$

$$Vs = Kp Cp Dp \left( \frac{Ts}{Ps Ms} \right)^{0.5} =$$

$$= ( 85.49 ) ( .800 ) ( 1.630 ) \left( \frac{1265.}{[ 30.028 ][ 28.395 ]} \right)^{0.5} = 135.8051$$

$$Qsd = 3600 ( 1 - Bws ) Vs A \frac{Tstd}{Ts} \frac{Ps}{Pstd} =$$

$$Qsd = 3600 ( 1 - .0598 ) ( 135.8051 ) ( 3.1416 ) \frac{( 528 ) ( 30.028 )}{( 1265. ) ( 29.92 )}$$

$$= 605066.4$$

# ETS

## METHOD 10 DATA SHEET

COMPANY Amoco Production SOURCE # 874 DATE 6/20/88  
 PARAMETER CO LOAD% MAX RUN NUMBER 1

### CALIBRATION STATISTICS

	Cylinder Value	Initial Analyzer Response		Final Analyzer Response		%Drift
		mv	ppm	mv	ppm	
Zero	<u>N/2</u>	<u>-20</u>	<u>1.54</u>	<u>-21</u>	<u>1.44</u>	<u>-0.1</u>
Low	<u>29.34</u>	<u>230</u>	<u>2748</u>	<u>227</u> <del><u>232</u></del>	<u>27.17</u>	<u>-0.3</u>
Mid	<u>59.76</u>	<u>535</u>	<u>59.14</u>	<u>535</u>	<u>59.14</u>	<u>0</u>
High	<u>89.85</u>	<u>840</u>	<u>90.8</u>	<u>842</u>	<u>91.0</u>	<u>0.2</u>

Calibration curve: ppm = (response mv)(slope) + intercept

Slope 0.10378 Intercept 3.61 Span Range 107.39

%Drift =  $\frac{\text{Final response (ppm)} - \text{Initial response (ppm)}}{\text{Span (ppm)}} \times 100$

### TEST DATA

Start time 8:45 Finish time 9:45 Minutes per point 7

Test Point mv Sample port A & B

1	<u>408</u>	11	_____	21	_____
2	<u>411</u>	12	_____	22	_____
3	<u>421</u>	13	_____	23	_____
4	<u>414</u>	14	_____	24	_____
5	<u>401</u>	15	_____	25	_____
6	<u>408</u>	16	_____	26	_____
7	<u>406</u>	17	_____	27	_____
8	<u>407</u>	18	_____	28	_____
9	_____	19	_____	29	_____
10	_____	20	_____	30	_____

Ave. mv 409.75

Ave. conc. 46.39 ppm

COMMENTS:



# ETS

## METHOD 10 DATA SHEET

COMPANY Amoco Production SOURCE # 87-4 DATE 6/28/88  
PARAMETER CO LOAD% MAX RUN NUMBER 2

### CALIBRATION STATISTICS

	Cylinder Value	Initial Analyzer Response		Final Analyzer Response		%Drift
		mv	ppm	mv	ppm	
Zero	<u>N2</u>	<u>-21</u>	<u>1.68</u>	<u>-18</u>	<u>1.99</u>	<u>0.3</u>
Low	<u>29.34</u>	<u>227</u>	<u>27.30</u>	<u>230</u>	<u>27.62</u>	<u>0.3</u>
Mid	<u>59.76</u>	<u>535</u>	<u>59.13</u>	<u>535</u>	<u>59.13</u>	<u>0</u>
High	<u>89.85</u>	<u>842</u>	<u>90.8</u>	<u>849</u>	<u>91.6</u>	<u>0.7</u>

Calibration curve:  $\text{ppm} = (\text{response mv})(\text{slope}) + \text{intercept}$

Slope 0.10332 Intercept 3.85 Span Range 107.17

%Drift =  $\frac{\text{Final response (ppm)} - \text{Initial response (ppm)}}{\text{Span (ppm)}} \times 100$

### TEST DATA

Start time 11:00 Finish time 12:00 Minutes per point 7

Test Point	mv	Sample port
1	<u>411</u>	_____
2	<u>405</u>	_____
3	<u>401</u>	_____
4	<u>401</u>	_____
5	<u>402</u>	_____
6	<u>405</u>	_____
7	<u>402</u>	_____
8	<u>404</u>	_____
9	_____	_____
10	_____	_____
11	_____	_____
12	_____	_____
13	_____	_____
14	_____	_____
15	_____	_____
16	_____	_____
17	_____	_____
18	_____	_____
19	_____	_____
20	_____	_____
21	_____	_____
22	_____	_____
23	_____	_____
24	_____	_____
25	_____	_____
26	_____	_____
27	_____	_____
28	_____	_____
29	_____	_____
30	_____	_____

Ave. mv 404.25

Ave. conc.  
45.616 ppm

COMMENTS:

# ETS

## METHOD 10 DATA SHEET

COMPANY Amoco Production SOURCE # 87-4 DATE 6/28/88  
 PARAMETER CO LOAD% ~~87.4~~ MAX RUN NUMBER 3

### CALIBRATION STATISTICS

	Cylinder Value	Initial Analyzer Response		Final Analyzer Response		%Drift
		mv	ppm	mv	ppm	
Zero	<u>N2</u>	<u>-18</u>	<u>1.80</u>	<u>-20</u>	<u>1.59</u>	<u>-0.2</u>
Low	<u>29.34</u>	<u>230</u>	<u>23.5</u>	<u>228</u>	<u>23.3</u>	<u>-0.2</u>
Mid	<u>59.76</u>	<u>535</u>	<u>57.6</u>	<u>540</u>	<u>58.2</u>	<u>0.5</u>
High	<u>89.85</u>	<u>849</u>	<u>92.7</u>	<u>852</u>	<u>92.8</u>	<u>0.1</u>

Calibration curve: ppm = (response mv)(slope) + intercept

Slope 0.102968 Intercept 3.65 Span Range 106.618

$$\%Drift = \frac{\text{Final response (ppm)} - \text{Initial response (ppm)}}{\text{Span (ppm)}} \times 100$$

### TEST DATA

Start time 13:00 Finish time 14:00 Minutes per point 7

Test Point	mv	Sample port
1	<u>422</u>	_____
2	<u>416</u>	_____
3	<u>418</u>	_____
4	<u>410</u>	_____
5	<u>401</u>	_____
6	<u>394</u>	_____
7	<u>404</u>	_____
8	<u>399</u>	_____
9	_____	_____
10	_____	_____
11	_____	_____
12	_____	_____
13	_____	_____
14	_____	_____
15	_____	_____
16	_____	_____
17	_____	_____
18	_____	_____
19	_____	_____
20	_____	_____
21	_____	_____
22	_____	_____
23	_____	_____
24	_____	_____
25	_____	_____
26	_____	_____
27	_____	_____
28	_____	_____
29	_____	_____
30	_____	_____

Ave. mv 407.625  
 Ave. conc. 45.626 ppm

COMMENTS:

Emission Testing Services, Inc.  
P.O. Box 15075  
Baton Rouge, LA 70895  
504-925-8405

Client : AMOCO  
Source : TURBINE  
Testing Date : 6-28-88

CARBON MONOXIDE EMISSION RATE

- ECO - Carbon Monoxide emission rate, lb/Hr
- F - Conversion factor for carbon monoxide, ( lb/ft<sup>3</sup> )/( PPM )  
( M<sub>CO</sub>/385 )/1,000,000 = 7.2727 X 10<sup>-8</sup>
- 385 - Volume of an ideal gas, ft<sup>3</sup>, at 528 deg R, 29.92 in-Hg
- M<sub>CO</sub> - Molecular weight of carbon monoxide, 28.00 lb/lb-mole
- CO<sub>ms</sub> - Concentration of CO as measured after scrubbing CO<sub>2</sub> - PPM
- CO<sub>2f</sub> - Concentration of CO<sub>2</sub> scrubbed from sample, %/100
- CO<sub>vV</sub> - Concentration of carbon monoxide, corr. for CO<sub>2</sub> - PPM
- CO<sub>wV</sub> - Concentration of carbon monoxide - lb/ft<sup>3</sup>
- Q<sub>sd</sub> - Dry volumetric stack gas flow rate, DSCF/Hr

CORRECTED CO CONCENTRATION FOR CO<sub>2</sub> SCRUBBED

$$CO_{vV} = CO_{ms} ( 1 - CO_{2f} )$$

----- RUN # 1 -----

$$CO_{vV} = ( 46.139 ) ( 1 - 0.024 ) = 45.032$$

$$CO_{wV} = CO_{vV} F = ( 45.032 ) ( 7.2727 \times 10^{-8} ) = 3.275 \times 10^{-6}$$

$$ECO = Q_{sd} CO_{wV} = ( 606692.7 ) ( 3.275 \times 10^{-6} ) = 1.987$$

----- RUN # 2 -----

$$CO_{vV} = ( 45.616 ) ( 1 - 0.024 ) = 44.521$$

$$CO_{wV} = CO_{vV} F = ( 44.521 ) ( 7.2727 \times 10^{-8} ) = 3.237 \times 10^{-6}$$

$$ECO = Q_{sd} CO_{wV} = ( 596727.0 ) ( 3.237 \times 10^{-6} ) = 1.932$$

----- RUN # 3 -----

$$CO_{vV} = ( 45.626 ) ( 1 - 0.024 ) = 44.531$$

$$CO_{wV} = CO_{vV} F = ( 44.531 ) ( 7.2727 \times 10^{-8} ) = 3.238 \times 10^{-6}$$

$$ECO = Q_{sd} CO_{wV} = ( 605066.4 ) ( 3.238 \times 10^{-6} ) = 1.960$$



METHOD 20 DATA SHEET

RESPONSE TIME TEST

COMPANY: Amoco Production SOURCE: Turbine #87-4  
DATE: JUNE 27, 1988 ANALYZER: TKleemox  
OPERATOR: [Signature] SPAN GAS: 13.13%

UPSCALE TIME

DOWNSCALE TIME

1) 70 sec.  
 52 sec.  
 52 sec.  
 54 sec.  
5) \_\_\_\_\_ sec.  
6) \_\_\_\_\_ sec.  
AVG. 52.67 sec.

1) 58 sec.  
 50 sec.  
 54 sec.  
 57 sec.  
5) \_\_\_\_\_ sec.  
6) \_\_\_\_\_ sec.  
AVG. 53.67 sec.

Greater Avg. = 53.67 sec.

Analyzer response time = 60+ avg.

ART = 114 sec.

## STATIONARY GAS TURBINE DATA SHEET

COMPANY Amoco Production SOURCE # 874 DATE 6/28/88  
 PARAMETER NOx LOAD% MAX RUN NUMBER 1

### CALIBRATION STATISTICS

	Cylinder Value	Initial Analyzer Response		Final Analyzer Response		%Drift
		mv	ppm	mv	ppm	
Zero	<u>N2</u>	<u>4</u>	<u>1.5</u>	<u>6</u>	<u>1.9</u>	<u>0.2</u>
Low	<u>40.82</u>	<u>182</u>	<u>40.6</u>	<u>186</u>	<u>41.5</u>	<u>0.4</u>
Mid	<u>79.81</u>	<u>351</u>	<u>77.7</u>	<u>349</u>	<u>77.3</u>	<u>-0.2</u>
High	<u>198.93</u>	<u>906</u>	<u>199.8</u>	<del>899</del> <u>902</u>	<u>198.9</u>	<u>-0.4</u>

Calibration curve: ppm = (response mv) (slope) + intercept

Slope 0.21986 Intercept 0.58 Span Range 220.44

%Drift =  $\frac{\text{Final response (ppm)} - \text{Initial response (ppm)}}{\text{Initial response (ppm)}} \times 100$

### TEST DATA

Temperature: WB 82 DB 89 BP \_\_\_\_\_

Start time 8:45 Finish time 9:45 Minutes per point 7

Sample port "A" : "B"

Test Point mv

1	<u>128</u>
2	<u>128</u>
3	<u>130</u>
4	<u>131</u>
5	<u>129</u>
6	<u>133</u>
7	<u>134</u>
8	<u>126</u>
average	_____ ppm <u>29.130</u>

R.H. = 74%

S.H. = 0.02225

COMMENTS: 129.875

## STATIONARY GAS TURBINE DATA SHEET

COMPANY Arrow Production SOURCE # 87-4 DATE 01/28/88  
PARAMETER NOx LOAD% MAX RUN NUMBER 2

## CALIBRATION STATISTICS

	Cylinder Value	Initial Analyzer Response		Final Analyzer Response		%Drift
		mv	ppm	mv	ppm	
Zero	<u>N2</u>	<u>6</u>	<u>1.28</u>	<u>9</u>	<u>1.95</u>	<u>0.3</u>
Low	<u>40.82</u>	<u>186</u>	<u>41.2</u>	<u>188</u>	<u>41.6</u>	<u>0.2</u>
Mid	<u>79.81</u>	<u>349</u>	<u>77.3</u>	<u>348</u>	<u>77.1</u>	<u>-0.1</u>
High	<u>198.93</u>	<u>902</u>	<u>199.82</u>	<u>899</u>	<u>199.16</u>	<u>-0.3</u>

Calibration curve: ppm = (response mv)(slope) + intercept

Slope 0.22159 Intercept -0.049 Span Range 221.541%Drift =  $\frac{\text{Final response (ppm)} - \text{Initial response (ppm)}}{\text{Initial response (ppm)}} \times 100$ 

## TEST DATA

Temperature: WB 85 DB 0101 BP \_\_\_\_\_Start time 11:00 Finish time 12:00 Minutes per point 7

Sample port \_\_\_\_\_

Test Point mv

1	<u>127</u>
2	<u>125</u>
3	<u>128</u>
4	<u>131</u>
5	<u>129</u>
6	<u>126</u>
7	<u>132</u>
8	<u>131</u>
average	_____ ppm <u>128.625</u>

R.H. = 52%

S.H. = 0.0226

COMMENTS: 128.625

## STATIONARY GAS TURBINE DATA SHEET

COMPANY Amoco Production SOURCE # 977-4 DATE 6/28/88  
 PARAMETER NOx LOAD% 100% RUN NUMBER 3

### CALIBRATION STATISTICS

	Cylinder Value	Initial Analyzer Response		Final Analyzer Response		%Drift
		mv	ppm	mv	ppm	
Zero	<u>N2</u>	<u>9</u>	<u>1.366</u>	<u>10</u>	<u>1.588</u>	<u>0.1</u>
Low	<u>4082</u>	<u>188</u>	<u>42.20</u>	<u>188</u>	<u>42.20</u>	<u>0</u>
Mid	<u>7981</u>	<u>348</u>	<u>77.59</u>	<u>347</u>	<u>77.37</u>	<u>-0.1</u>
High	<u>19893</u>	<u>899</u>	<u>199.5</u>	<u>896</u>	<u>198.8</u>	<u>-0.3</u>

Calibration curve: ppm = (response mv)(slope) + intercept

Slope 0.22308 Intercept -0.643 Span Range 222.437

%Drift =  $\frac{\text{Final response (ppm)} - \text{Initial response (ppm)}}{\text{Initial response (ppm)}} \times 100$

### TEST DATA

Temperature: WB 86 DB 103 BP \_\_\_\_\_

Start time 13:00 Finish time 14:00 Minutes per point 2

Sample port \_\_\_\_\_

Test Point mv

1	<u>132</u>	
2	<u>131</u>	
3	<u>133</u>	
4	<u>128</u>	
5	<u>126</u>	
6	<u>131</u>	
7	<u>128</u>	
8	<u>127</u>	
average	<u>129.5</u>	ppm <u>28,246</u>

COMMENTS:



Emission Testing Services, Inc.  
P.O. Box 15075  
Baton Rouge, LA 70895  
504-925-8405

Client : AMOCO  
Source : TURBINE  
Testing Date : 6-28-88

OXIDES OF NITROGEN EMISSION RATE - SUBPART GG

- ENOX - Oxides of nitrogen as NO<sub>2</sub>, emission rate, lb/Hr
- F - Conversion factor for NO<sub>2</sub>, 1.1948 X 10<sup>-7</sup> ( lb/ft<sup>3</sup> )/(PPM)
- NOX<sub>vv</sub> - NOX Conc. as NO<sub>2</sub>, ISO conditions, PPM
- NOX<sub>wv</sub> - NOX Conc. as NO<sub>2</sub>, ISO conditions, lb/ ft<sup>3</sup>
- Q<sub>sd</sub> - Dry volumetric stack gas flow rate, DSCF/Hr
- CONC<sub>c</sub> - NOX conc. as measured, PPM
- P<sub>ref</sub> - Reference combustor inlet pressure, at ISO conditions, supplied by Turbine manufacturer, Kilopascals absolute
- P<sub>obs</sub> - Measured combustor inlet pressure, Kilopascals absolute
- H<sub>obs</sub> - Specific humidity of ambient air, lb H<sub>2</sub>O/ lb dry air
- T<sub>amb</sub> - Measured ambient temperature, DEG. K

CORRECTION TO ISO STANDARD DAY CONDITIONS

$$NOX_{vv} = CONC_c \left( \frac{P_{ref}}{P_{obs}} \right)^{0.5} \left( e^{19(H_{obs} - 0.00633)} \right) \left( \frac{288}{T_{amb}} \right)^{1.53}$$

----- RUN # 1 -----

$$NOX_{vv} = (29.130) \left( \frac{496.4}{464.2} \right)^{0.5} \left( e^{19(0.0222 - 0.00633)} \right) \left( \frac{288}{304.7} \right)^{1.53} =$$

$$NOX_{wv} = NOX_{vv} F = (35.536) (1.1948 \times 10^{-7}) = 4.245 \times 10^{-6}$$

$$ENOX = Q_{sd} NOX_{wv} = (606692.7) (4.245 \times 10^{-6}) = 2.576$$

----- RUN # 2 -----

$$NOX_{vv} = (28.453) \left( \frac{496.4}{455.1} \right)^{0.5} \left( e^{19(0.0244 - 0.00633)} \right) \left( \frac{288}{312.4} \right)^{1.53} =$$

$$NOX_{wv} = NOX_{vv} F = (34.939) (1.1948 \times 10^{-7}) = 4.174 \times 10^{-6}$$

$$ENOX = Q_{sd} NOX_{wv} = (596727.0) (4.174 \times 10^{-6}) = 2.491$$

----- RUN # 3 -----

$$NOX_{vv} = (28.246) \left( \frac{496.4}{452.3} \right)^{0.5} \left( e^{19(0.0232 - 0.00633)} \right) \left( \frac{288}{312.4} \right)^{1.53} =$$

$$NOX_{wv} = NOX_{vv} F = (34.137) (1.1948 \times 10^{-7}) = 4.078 \times 10^{-6}$$

$$ENOX = Q_{sd} NOX_{wv} = (605066.4) (4.078 \times 10^{-6}) = 2.468$$

Emission Testing Services, Inc.  
P.O. Box 15075  
Baton Rouge, LA 70895  
504-925-8405

Client : AMOCO  
Source : TURBINE  
Testing Date : 6-28-88

OXIDES OF NITROGEN CONCENTRATION

CORRECTED TO 15 % OXYGEN - ISO STANDARD DAY CONDITIONS

CORRECTION TO 15 % OXYGEN

CONC<sub>meas</sub> - NOX concentration as measured, Corr. to ISO, PPM  
CONC<sub>c</sub> - NOX concentration corrected to 15% OXYGEN, PPM  
O<sub>2</sub><sub>conc</sub> - Measured oxygen concentration, %

$$\text{CONC}_c = \text{CONC}_{\text{meas}} \frac{20.9}{20.9 - \text{O}_2_{\text{conc}}}$$

----- RUN # 1 -----

$$\text{CONC}_c = ( 35.536 ) \frac{20.9}{20.9 - ( 16.9 )} = 52.416$$

----- RUN # 2 -----

$$\text{CONC}_c = ( 34.939 ) \frac{20.9}{20.9 - ( 17.0 )} = 52.856$$

----- RUN # 3 -----

$$\text{CONC}_c = ( 34.137 ) \frac{20.9}{20.9 - ( 16.8 )} = 49.124$$

VISIBLE EMISSION OBSERVATION FORM

**SOURCE NAME**  
Co-Generation Turbine

**ADDRESS**  
Amoco Production Company  
Rt 1A Box 42

**CITY** Morganza **STATE** LA **ZIP** 70759

**PHONE** (24) 694-3630 **SOURCE ID NUMBER** 87-4

**PROCESS EQUIPMENT**  
Turbine Generator **OPERATING MODE** MAX

**CONTROL EQUIPMENT**  
N/A **OPERATING MODE** N/A

**DESCRIBE EMISSION POINT**  
RT 1' Above stack **STOP** SAME

**HEIGHT ABOVE GROUND LEVEL**  
START 30' **STOP** SAME **HEIGHT RELATIVE TO OBSERVER**  
START 24.2' **STOP** SAME

**DISTANCE FROM OBSERVER**  
RT 200' **STOP** 200' **DIRECTION FROM OBSERVER**  
START WEST **STOP** SAME

**DESCRIBE EMISSIONS**  
RT NONE **STOP** NONE

**EMISSION COLOR**  
START N/A **STOP** SAME **PLUME TYPE** CONTINUOUS  FUGITIVE  INTERMITTENT

**WATER DROPLETS PRESENT**  
NO  YES  **IS WATER DROPLET PLUME**  
ATTACHED  DETACHED

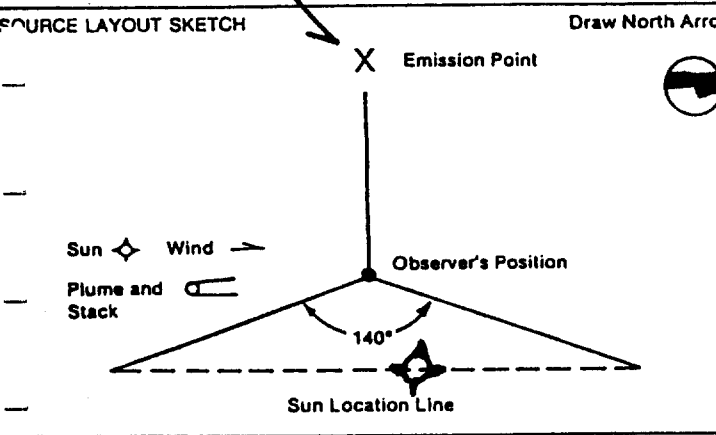
**POINT IN THE PLUME AT WHICH OPACITY WAS DETERMINED**  
START N/A **STOP** SAME

**DESCRIBE BACKGROUND**  
START Hazy **STOP** SAME

**BACKGROUND COLOR**  
START Gray **STOP** SAME **SKY CONDITIONS**  
START CLEAR **STOP** SAME

**WIND SPEED**  
START 3MPH **STOP** 5MPH **WIND DIRECTION**  
START WSW **STOP** SAME

**WET BULB TEMP** 83°F **STOP** 85°F **WET BULB TEMP** 82°F **RH, percent** 74%



**REMARKS**

**I HAVE RECEIVED A COPY OF THESE OPACITY OBSERVATIONS**

**SIGNATURE**

**TITLE**

**DATE**

OBSERVATION DATE					START TIME		STOP TIME			
062888					0845		0905			
MIN	SEC				MIN	SEC				
	0	15	30	45		0	15	30	45	
1	0	0	0	0	31					
2	0	0	0	0	32					
3	0	0	0	0	33					
4	0	0	0	0	34					
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18	0	0	0	0	48					
19	0	0	0	0	49					
20	0	0	0	0	50					
21					51					
22					52					
23					53					
24					54					
25					55					
26					56					
27					57					
28					58					
29					59					
30					60					

**AVERAGE OPACITY FOR HIGHEST PERIOD** 0 **NUMBER OF READINGS ABOVE % WERE** 0

**RANGE OF OPACITY READINGS**  
0 **MINIMUM** 0 **MAXIMUM**

**OBSERVER'S NAME (PRINT)**  
JOHN R. ANGELLOZ, JR.

**OBSERVER'S SIGNATURE**  
John R. Angelloz, Jr. **DATE** 062888

**ORGANIZATION**  
EMISSIONS TESTING SERVICES

**CERTIFIED BY**  
Louisiana D.E.Q. **DATE** 042188

**VERIFIED BY**  
J. GIPSON **DATE** 042188

VISIBLE EMISSION OBSERVATION FORM

SOURCE NAME  
**Co-Generation Turbine**

ADDRESS  
**AMOCO PRODUCTION COMPANY**

**Rt 1A Box 42**

CITY STATE ZIP  
**Morganza LA 70759**

PHONE SOURCE ID NUMBER  
**(504) 694-3630 87-4**

PROCESS EQUIPMENT OPERATING MODE  
**Turbine Generator MAX**

CONTROL EQUIPMENT OPERATING MODE  
**N/A N/A**

DESCRIBE EMISSION POINT

HEIGHT ABOVE GROUND LEVEL START **30'** STOP **SAME**

HEIGHT RELATIVE TO OBSERVER START **24.2'** STOP **SAME**

DIRECTION FROM OBSERVER START **WEST** STOP **SAME**

DESCRIBE EMISSIONS

RT **NONE** STOP **NONE**

EMISSION COLOR START **N/A** STOP **SAME**

PLUME TYPE CONTINUOUS  FUGITIVE  INTERMITTENT

WATER DROPLETS PRESENT NO  YES  IS WATER DROPLET PLUME ATTACHED  DETACHED

POINT IN THE PLUME AT WHICH OPACITY WAS DETERMINED START **N/A** STOP **SAME**

DESCRIBE BACKGROUND

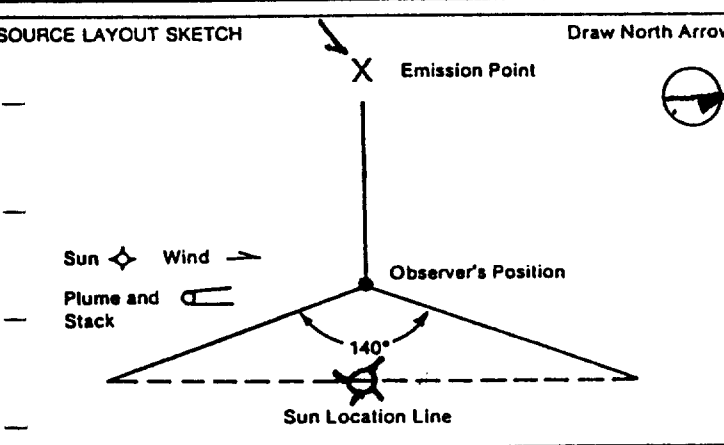
START **HAZY** STOP **SAME**

BACKGROUND COLOR START **Gray** STOP **SAME**

WIND SPEED START **3MPH** STOP **SAME**

WIND DIRECTION START **SW** STOP **SAME**

WET BULB TEMP RH, percent START **90°F** STOP **92°F** **85°F** **52**



COMMENTS

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SIGNATURE

TITLE

DATE

OBSERVATION DATE					START TIME		STOP TIME			
062888					1100		1120			
SEC	0	15	30	45	SEC	0	15	30	45	
MIN					MIN					
1	0	0	0	0	31					
2	0	0	0	0	32					
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21					51					
22					52					
23					53					
24					54					
25					55					
26					56					
27					57					
28					58					
29					59					
30					60					

AVERAGE OPACITY FOR HIGHEST PERIOD 0

NUMBER OF READINGS ABOVE 0 % WERE 0

RANGE OF OPACITY READINGS

0 MINIMUM 0 MAXIMUM

OBSERVER'S NAME (PRINT)  
**JOHN R. ANGELLOZ, JR.**

OBSERVER'S SIGNATURE  
*John R. Angelloz, Jr.* DATE **062888**

ORGANIZATION  
**EMISSIONS TESTING SERVICES**

CERTIFIED BY  
**LOUISIANA D.E.R.** DATE **042188**

VERIFIED BY  
**J. GIPSON** DATE **042188**

VISIBLE EMISSION OBSERVATION FORM

SOURCE NAME  
**Co-Generation Turbine**

ADDRESS  
**Amoco Production Company**

**Rt 1A Box 42**

CITY STATE ZIP  
**Morganza LA 70759**

PHONE SOURCE ID NUMBER  
**(504) 694-3630 87-4**

PROCESS EQUIPMENT OPERATING MODE  
**Turbine Generator MAX**

CONTROL EQUIPMENT OPERATING MODE  
**N/A N/A**

DESCRIBE EMISSION POINT

START **1' Above Stack** STOP **SAME**

HEIGHT ABOVE GROUND LEVEL HEIGHT RELATIVE TO OBSERVER  
START **30'** STOP **SAME** START **24.2'** STOP **SAME**

DISTANCE FROM OBSERVER DIRECTION FROM OBSERVER  
START **200'** STOP **200'** START STOP **SAME**

DESCRIBE EMISSIONS

START **NONE** STOP **NONE**

EMISSION COLOR PLUME TYPE CONTINUOUS   
START **N/A** STOP **SAME** FUGITIVE  INTERMITTENT

WATER DROPLETS PRESENT IS WATER DROPLET PLUME  
NO  YES  ATTACHED  DETACHED

POINT IN THE PLUME AT WHICH OPACITY WAS DETERMINED  
START **N/A** STOP **SAME**

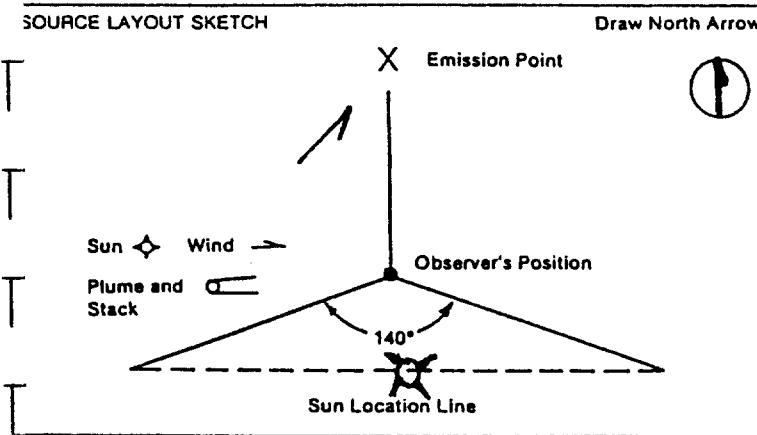
DESCRIBE BACKGROUND

START **BLUE SKY** STOP **SAME**

BACKGROUND COLOR SKY CONDITIONS  
START **BLUE** STOP **SAME** START **clear** STOP **SAME**

WIND SPEED WIND DIRECTION  
START **3MPH** STOP **SAME** START **WSW** STOP **SAME**

AMBIENT TEMP WET BULB TEMP RH, percent  
START **96°F** STOP **98°F** **86°F** **50**



COMMENTS

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SIGNATURE TITLE DATE

OBSERVATION DATE					START TIME		STOP TIME				
062888					1300		1320				
MIN	SEC	0	15	30	45	MIN	SEC	0	15	30	45
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21						51					
22						52					
23						53					
24						54					
25						55					
26						56					
27						57					
28						58					
29						59					
30						60					

AVERAGE OPACITY FOR HIGHEST PERIOD **0** NUMBER OF READINGS ABOVE **0** % WERE **0**

RANGE OF OPACITY READINGS **0** MINIMUM **0** MAXIMUM

OBSERVER'S NAME (PRINT)  
**JOHN R. ANGELLOZ, JR.**

OBSERVER'S SIGNATURE DATE  
*John R. Angelloz, Jr.* **062888**

ORGANIZATION  
**EMISSIONS TESTING SERVICES**

CERTIFIED BY DATE  
**Louisiana D.E.Q.** **042188**

VERIFIED BY DATE  
**J. GIPSON** **042188**

## METHOD 6C & 7E DATA SHEET

COMPANY Amoco Production SOURCE # 874 DATE 6/28/80

PARAMETER D<sub>2</sub> LOAD% MAX RUN NUMBER 1

### CALIBRATION STATISTICS

Cylinder	Value	Analyzer mv	Response ppm	Absolute mv	Difference ppm	% Span +2%
Zero	<u>N<sub>2</sub></u>	<u>0.23</u>	<u>0.003</u>	<u>0.23</u>	<u>0.003</u>	<u>0</u>
Mid	<u>13.13</u>	<u>5.38</u>	<u>13.12</u>	<u>5.36</u>	<u>13.07</u>	<u>-0.2</u>
High	<u>19.89</u>	<u>8.04</u>	<u>19.90</u>	<u>8.04</u>	<u>19.90</u>	<u>0</u>

Calibration curve: ppm = (response mv)(slope) + intercept

Slope 2.5471 Intercept -0.583 Span Range 24.888

Analyzer Cal mv	Init. Analyzer ppm	Analyzer Resp. Bias +5	Final Analyzer mv	Final Analyzer ppm	Bias +5	Span +3	Drift
-----------------	--------------------	------------------------	-------------------	--------------------	---------	---------	-------

Conc. N/A

Sys. Cal. Bias =  $\frac{\text{Sys. cal. (ppm)} - \text{analyzer cal. (ppm)} \times 100}{\text{Span (ppm)}}$

%Drift =  $\frac{\text{Final sys. resp. (ppm)} - \text{Initial sys. resp. (ppm)} \times 100}{\text{span (ppm)}}$

### TEST DATA

Start time 8:45 Finish time 9:45 Minutes per point 7

Test Point mv Sample port A: B

1	<u>6.84</u>	11	_____	21	_____
2	<u>6.81</u>	12	_____	22	_____
3	<u>6.80</u>	13	_____	23	_____
4	<u>6.79</u>	14	_____	24	_____
5	<u>6.77</u>	15	_____	25	_____
6	<u>6.74</u>	16	_____	26	_____
7	<u>6.78</u>	17	_____	27	_____
8	<u>6.79</u>	18	_____	28	_____
9	_____	19	_____	29	_____
10	_____	20	_____	30	_____

Ave. mv 6.79  
Ave. conc. 16.712 ppm %

COMMENTS:

# ETS

## METHOD 6C & 7E DATA SHEET

COMPANY Amoco Production SOURCE # 87-4 DATE 6/28/88  
PARAMETER O<sub>2</sub> LOAD% MAX RUN NUMBER 2

### CALIBRATION STATISTICS

Cylinder Value	Analyzer Response		Absolute Difference		% Span +2%
	mv	ppm	mv	ppm	
Zero <u>N<sub>2</sub></u>	<u>0.23</u>	<u>0.014</u>	<u>0.23</u>	<u>0.014</u>	<u>0</u>
Mid <u>13.13</u>	<u>5.36</u>	<u>13.09</u>	<u>5.37</u>	<u>13.11</u>	<u>0.1</u>
High <u>19.99</u>	<u>8.04</u>	<u>19.92</u>	<u>8.04</u>	<u>19.92</u>	<u>0</u>

Calibration curve: ppm = (response mv)(slope) + intercept

Slope 2.5484 Intercept -0.572 Span Range 24.912

Analyzer Cal	Init. Analyzer	Analyzer Resp.	Final Analyzer	Analyzer Resp.	Span	Drift
mv	ppm	Bias +5	mv	ppm	Bias +5	+3

Conc. N/A

Sys. Cal. Bias =  $\frac{\text{Sys. cal. (ppm)} - \text{analyzer cal. (ppm)}}{\text{Span (ppm)}} \times 100$

%Drift =  $\frac{\text{Final sys. resp. (ppm)} - \text{Initial sys. resp. (ppm)}}{\text{span (ppm)}} \times 100$

### TEST DATA

Start time 11:00 Finish time 12:00 Minutes per point 7

Test Point	mv	Sample port
1	<u>6.80</u>	
2	<u>6.81</u>	
3	<u>6.79</u>	
4	<u>6.82</u>	
5	<u>6.80</u>	
6	<u>6.84</u>	
7	<u>6.75</u>	
8	<u>6.79</u>	
9		
10		
11		
12		
13		
14		
15		
16		
17		
18		
19		
20		
21		
22		
23		
24		
25		
26		
27		
28		
29		
30		

Ave. mv 6.800  
Ave. conc. 16.758 ppm

COMMENTS:

# ETS

## METHOD 6C & 7E DATA SHEET

COMPANY Amoco Production SOURCE # 87-4 DATE 6/28/88  
 PARAMETER O<sub>2</sub> LOAD% \_\_\_\_\_ RUN NUMBER 3

### CALIBRATION STATISTICS

Cylinder Value	Analyzer Response mv	Response ppm	Absolute mv	Difference ppm	% Span +2%
Zero <u>N<sub>2</sub></u>	<u>0.23</u>	<u>0.009</u>	<u>0.23</u>	<u>0.009</u>	<u>0</u>
Mid <u>13.13</u>	<u>5.37</u>	<u>13.10</u>	<u>5.35</u>	<u>13.05</u>	<u>-0.2</u>
High <u>19.89</u>	<u>8.04</u>	<u>19.76</u>	<u>8.05</u>	<u>19.78</u>	<u><del>0.0</del> 0.1</u>

Calibration curve: ppm = (response mv)(slope) + intercept

Slope 2.5478 Intercept -0.577 Span Range 24.901

Analyzer Cal	Init. Analyzer mv	Analyzer Resp. ppm	Bias +5	Final Analyzer mv	Final Analyzer ppm	Bias +5	Span	Drift +3
Conc. _____	_____	_____	_____	_____	_____	_____	_____	_____

$$\text{Sys. Cal. Bias} = \frac{\text{Sys. cal. (ppm)} - \text{analyzer cal. (ppm)}}{\text{Span (ppm)}} \times 100$$

$$\% \text{Drift} = \frac{\text{Final sys. resp. (ppm)} - \text{Initial sys. resp. (ppm)}}{\text{span (ppm)}} \times 100$$

### TEST DATA

Start time 13:00 Finish time 14:00 Minutes per point 17

Test Point	mv		Sample port
1	<u>6.77</u>	11	_____
2	<u>6.74</u>	12	_____
3	<u>6.77</u>	13	_____
4	<u>6.76</u>	14	_____
5	<u>6.74</u>	15	_____
6	<u>6.76</u>	16	_____
7	<u>6.76</u>	17	_____
8	<u>6.87</u>	18	_____
9	_____	19	_____
10	_____	20	_____
		21	_____
		22	_____
		23	_____
		24	_____
		25	_____
		26	_____
		27	_____
		28	_____
		29	_____
		30	_____

Ave. mv 6.7638

Ave. conc. 16.655 ppm %

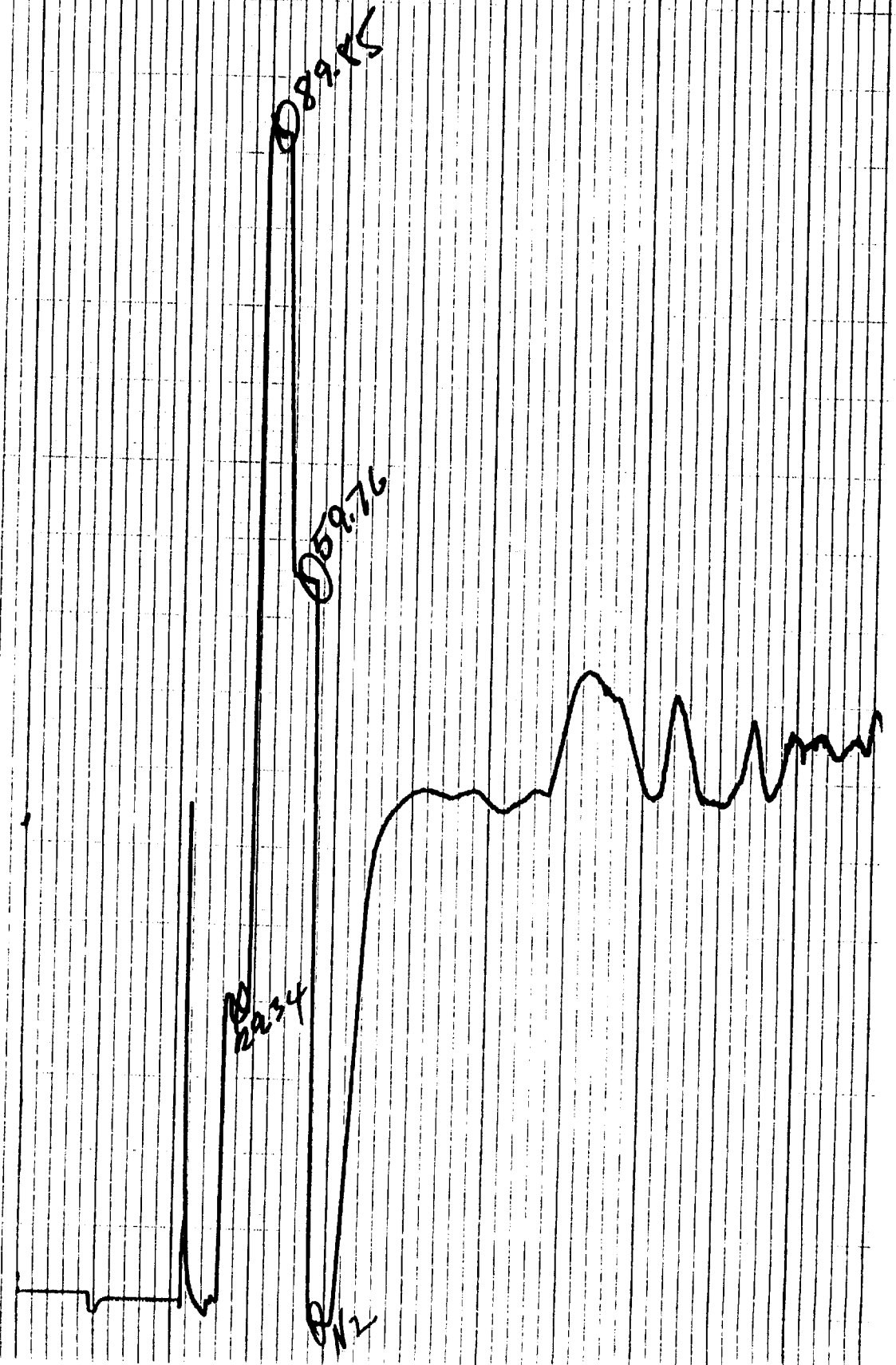
COMMENTS:

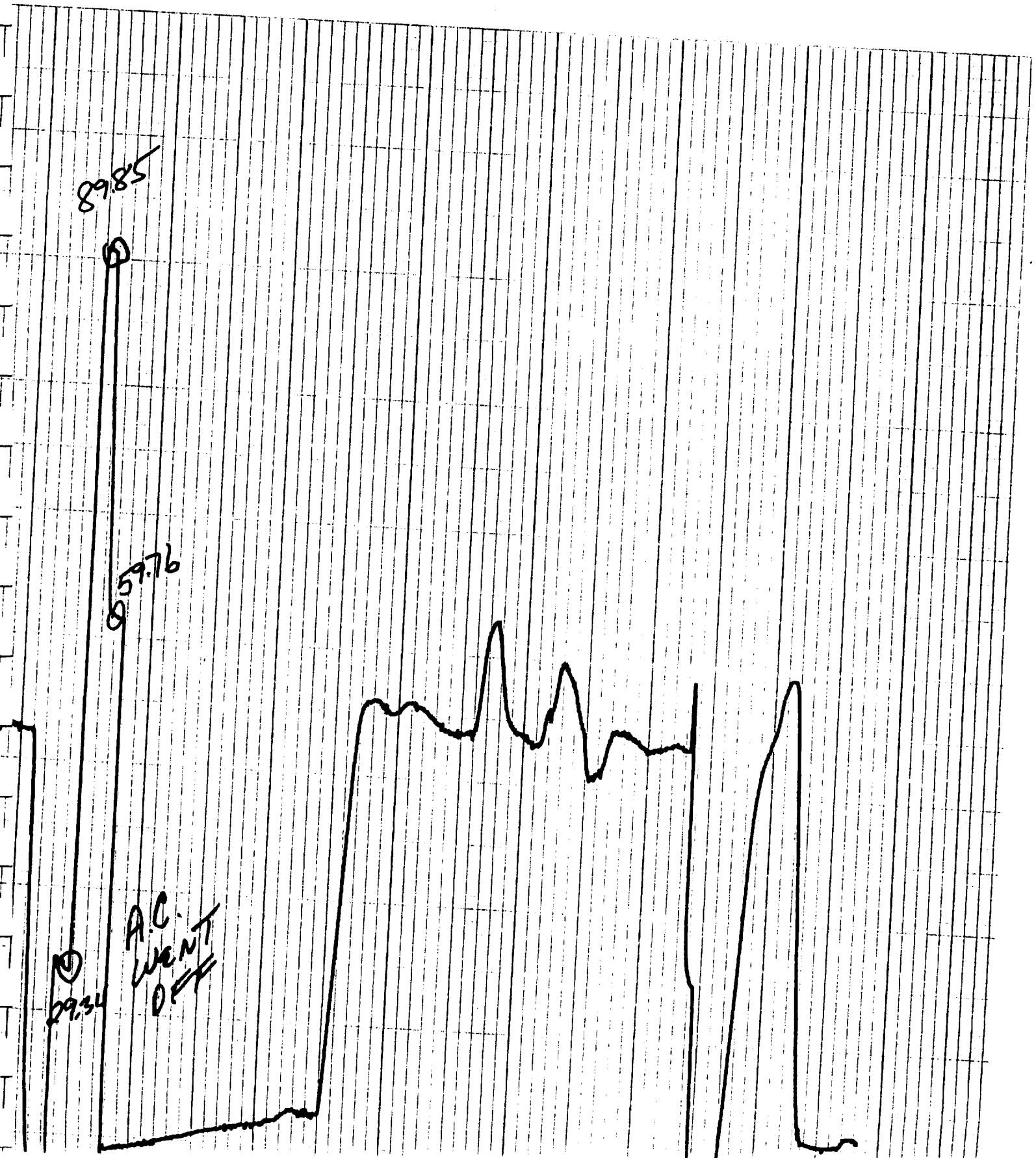


Amoco  
Production  
CO

6/27/88

SETUP  
MONDAY





noce  
duction

6/25/88

Carbonyl  
Nitroxide

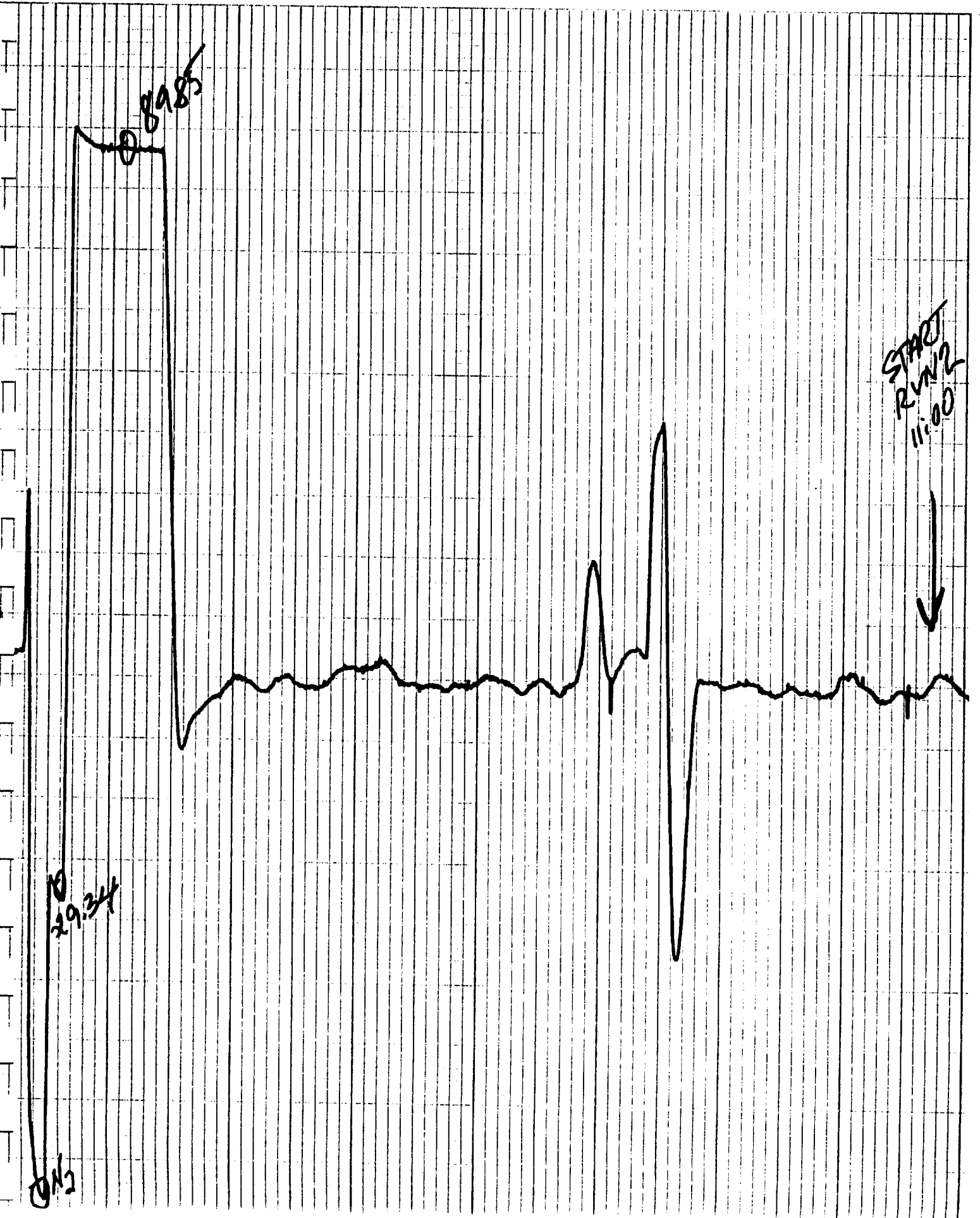


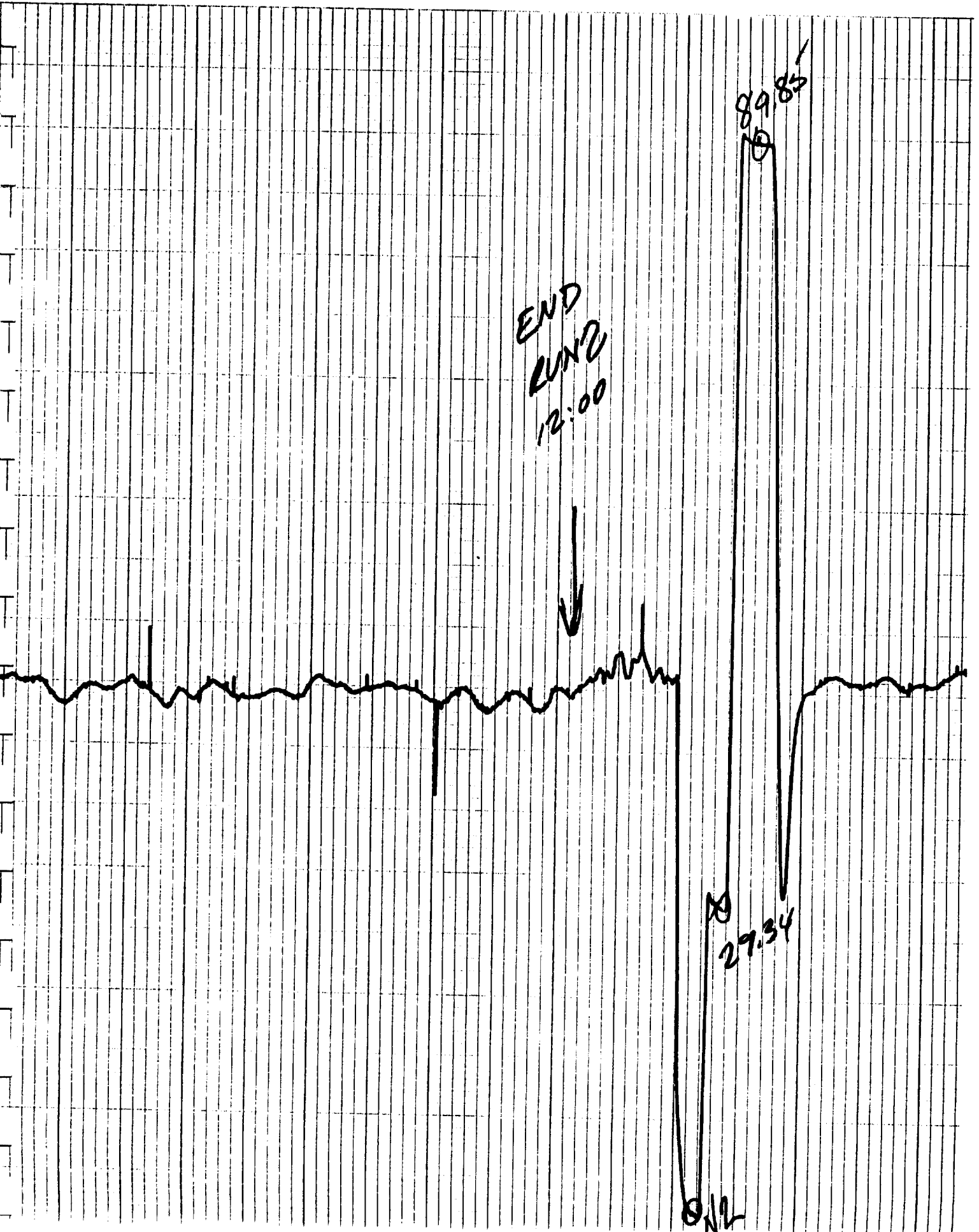
UN  
ACK

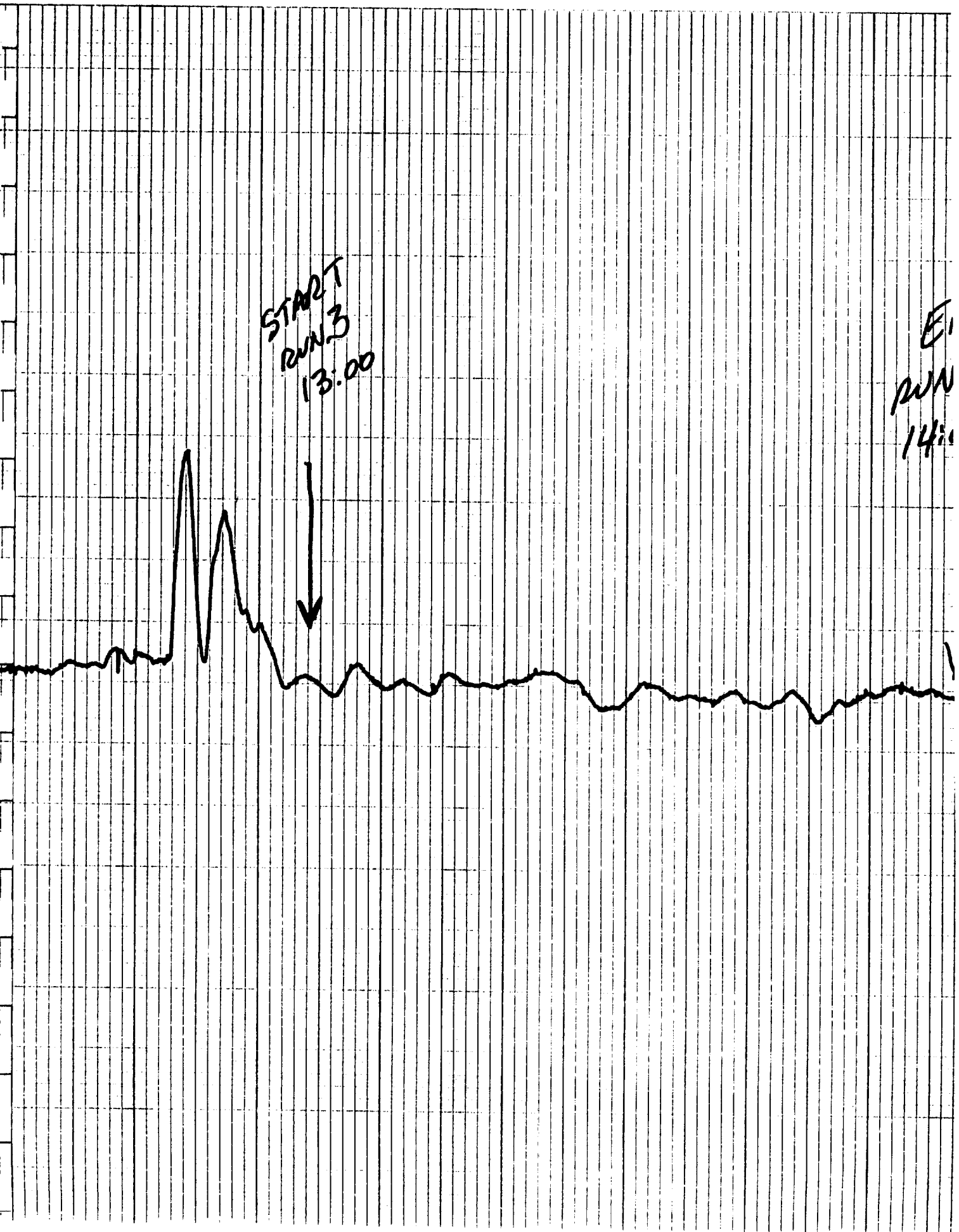
START  
RUN # 1  
8:46



↑  
END  
RUN # 1  
9:45







START  
RUN 3  
13:00

E  
RUN  
14:00

59.85

59.76

29.34

QW2

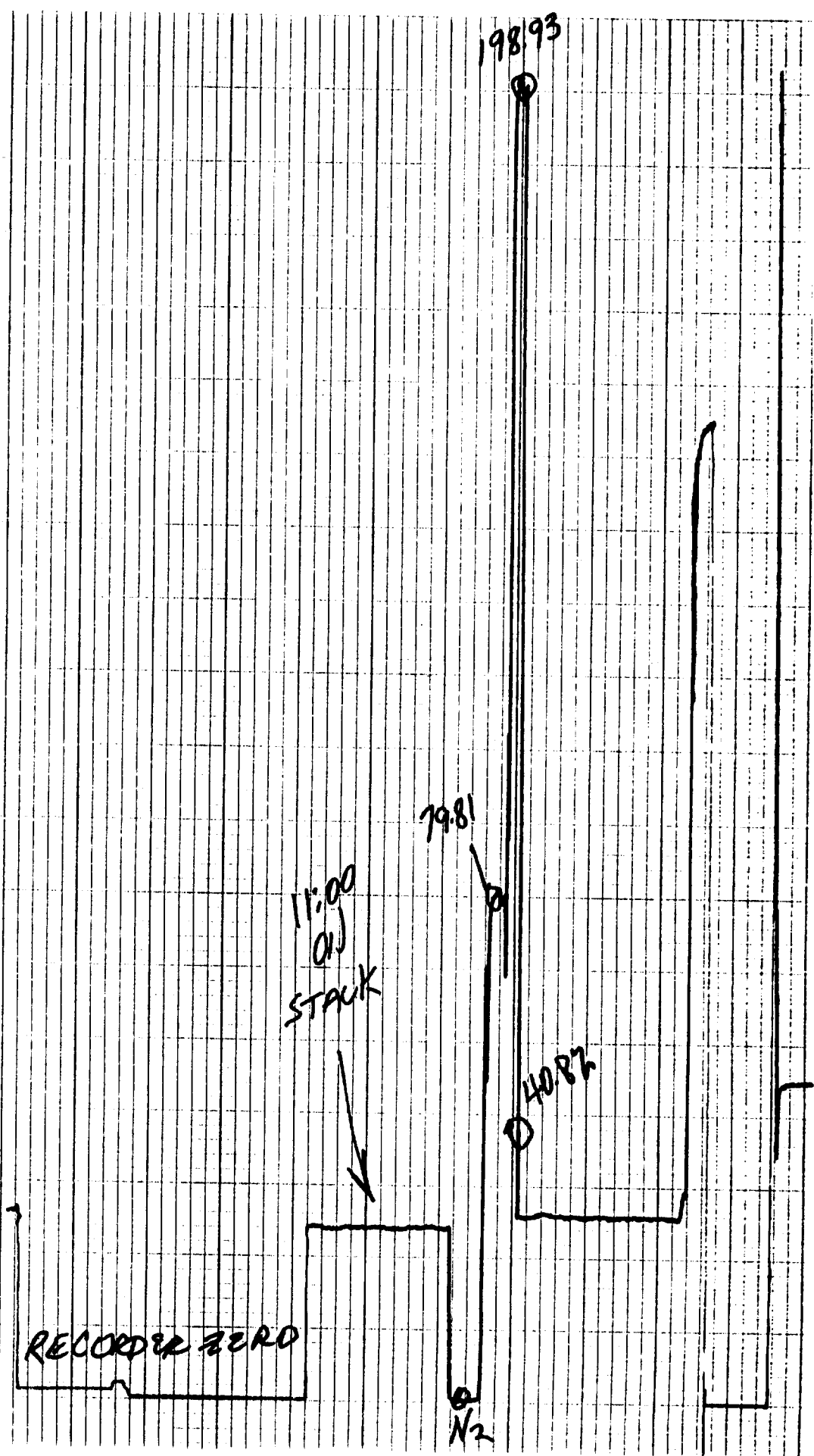


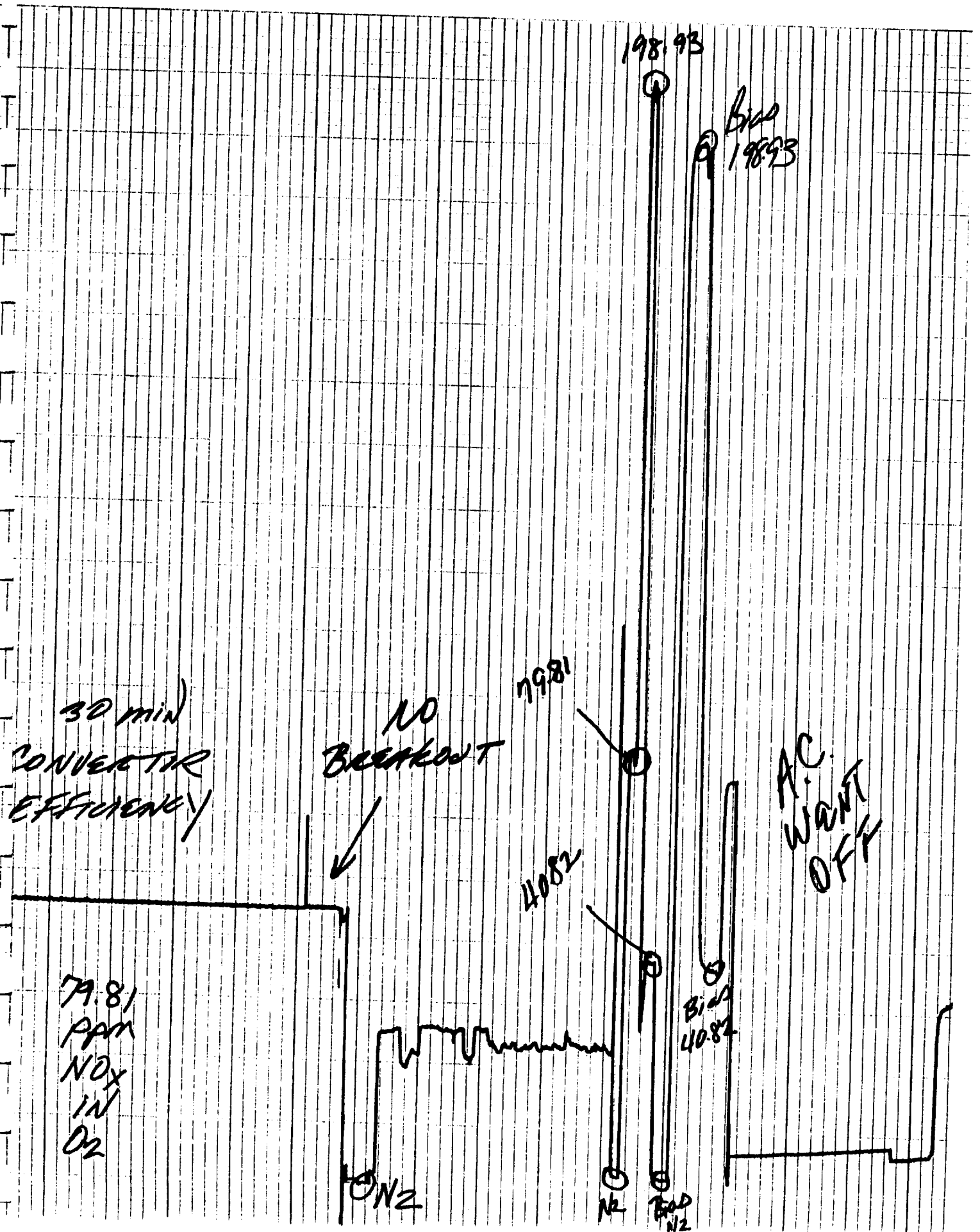
Amoco  
Production

N<sub>2</sub>X

6/27/89

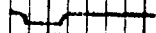
SETUP  
Manning

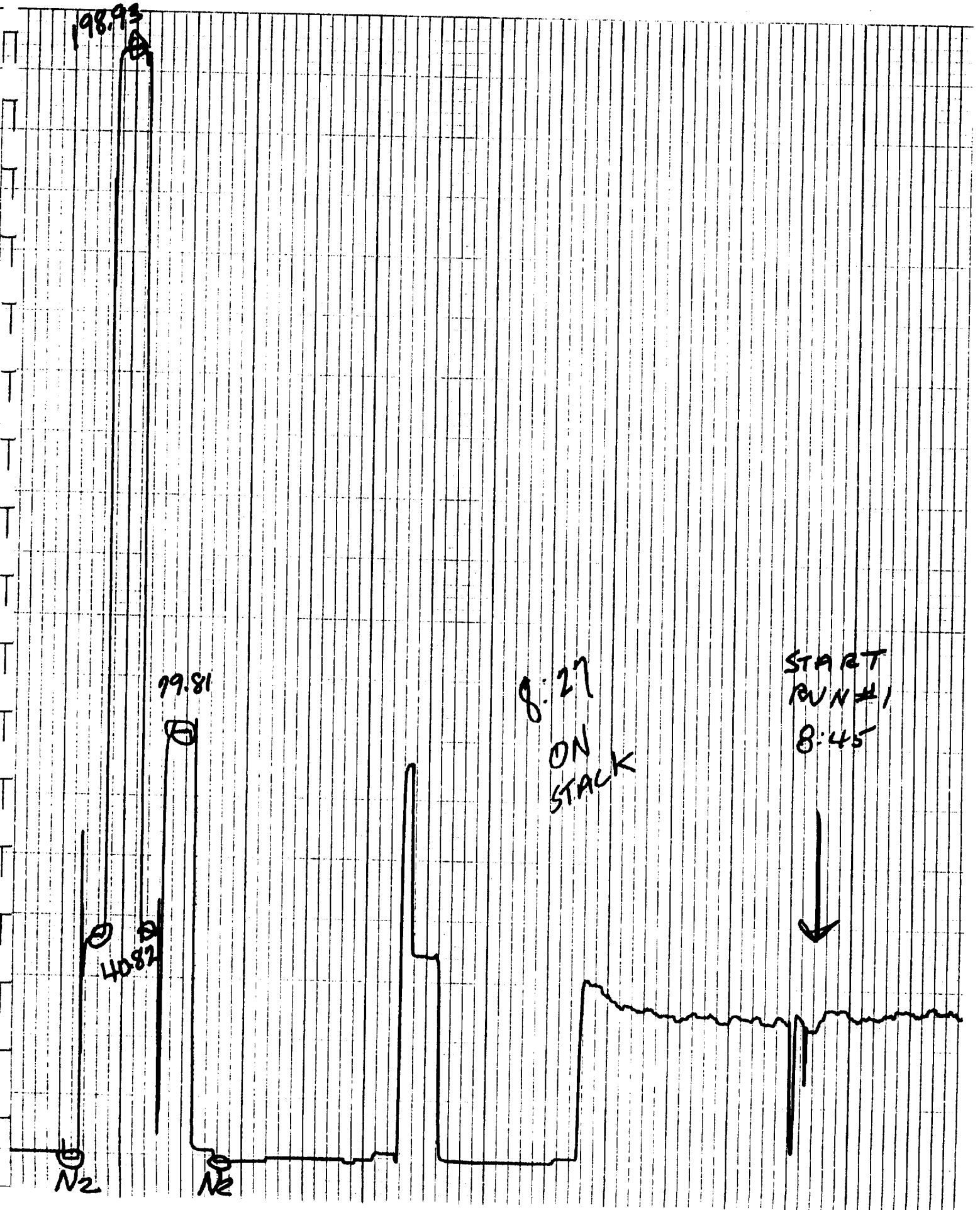


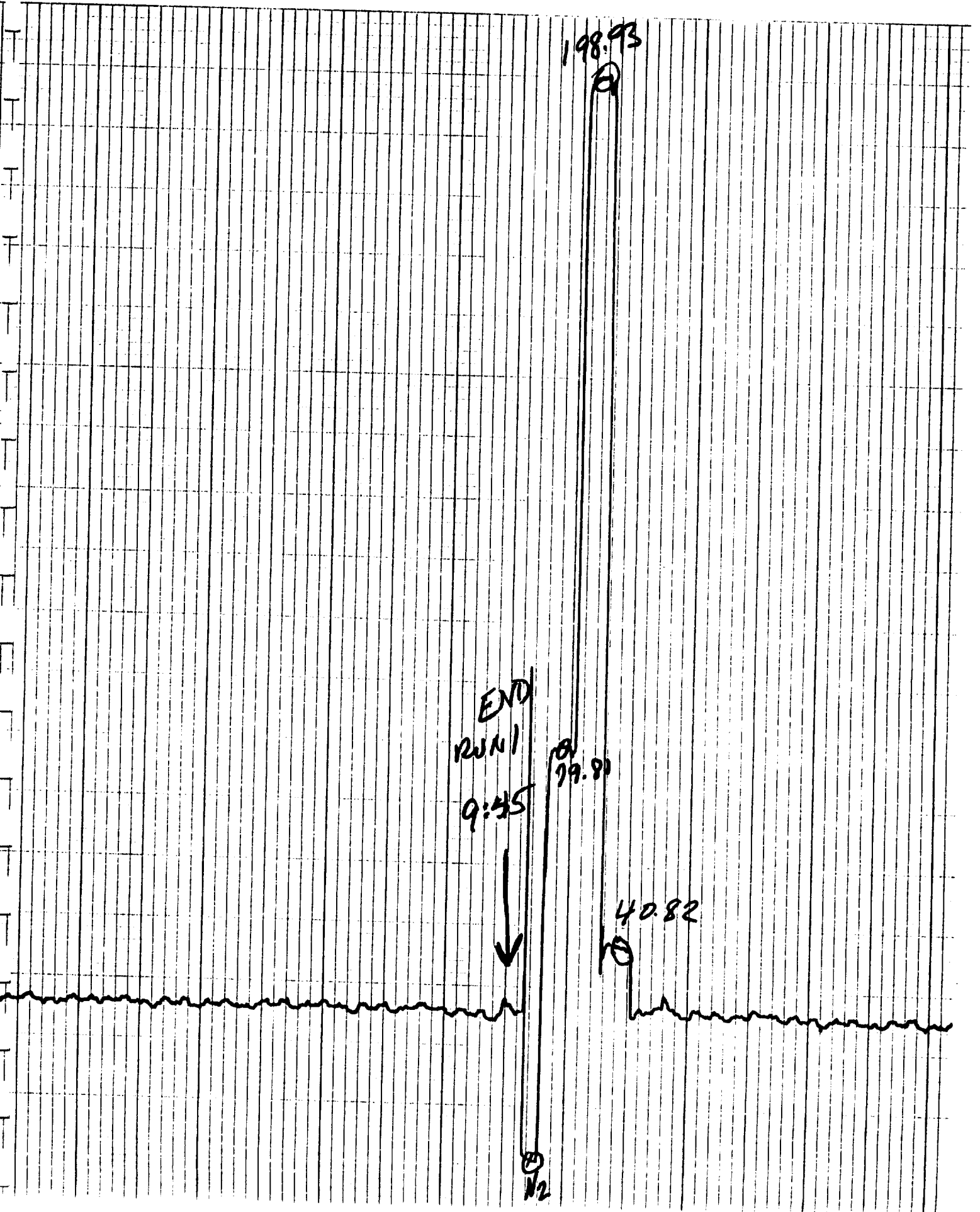


Amoco  
Production  
6/23/88

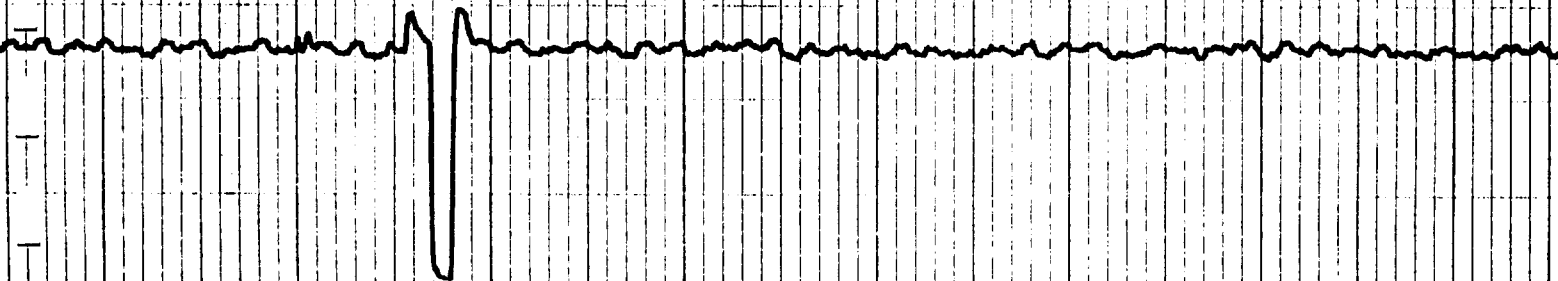
NOx

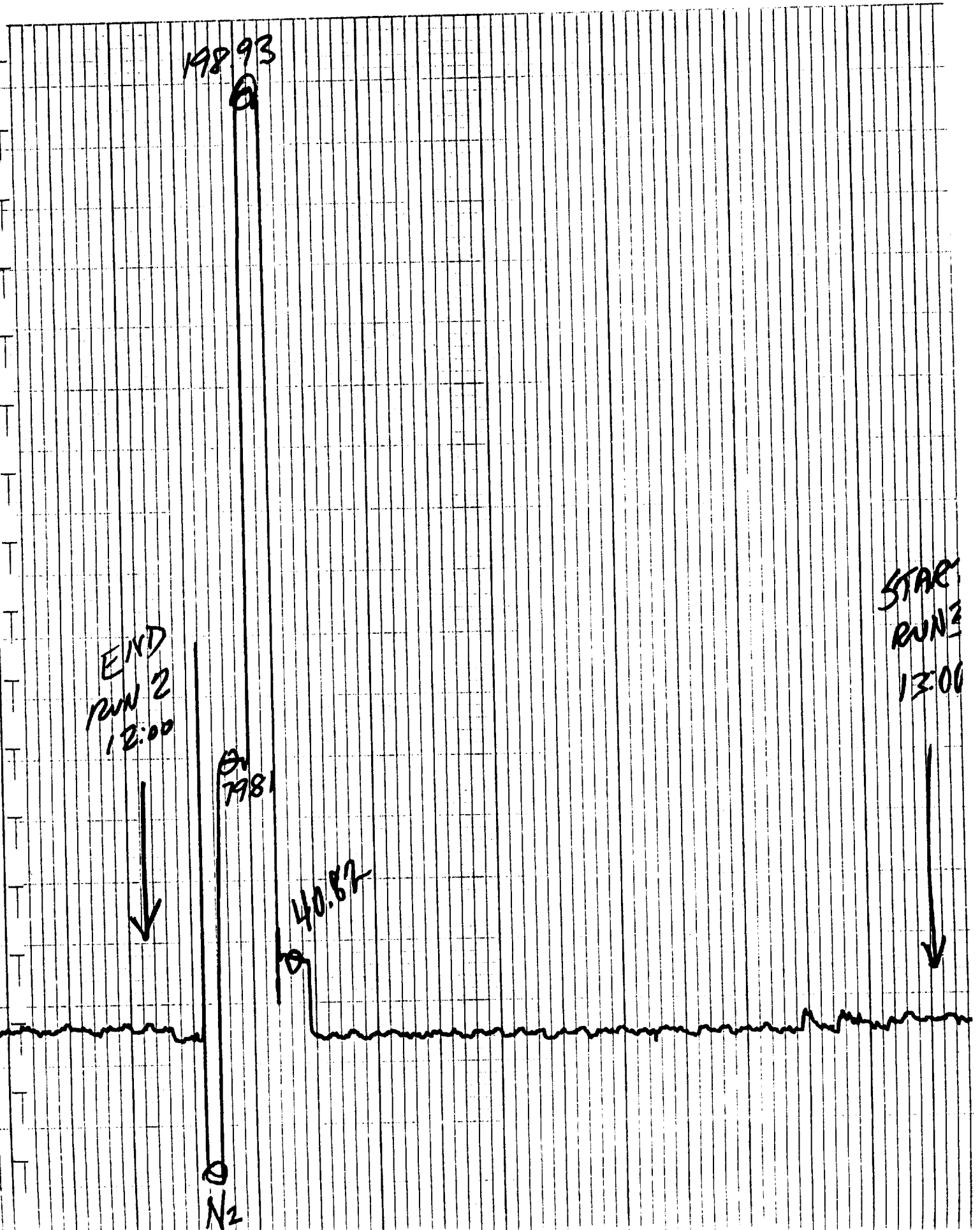


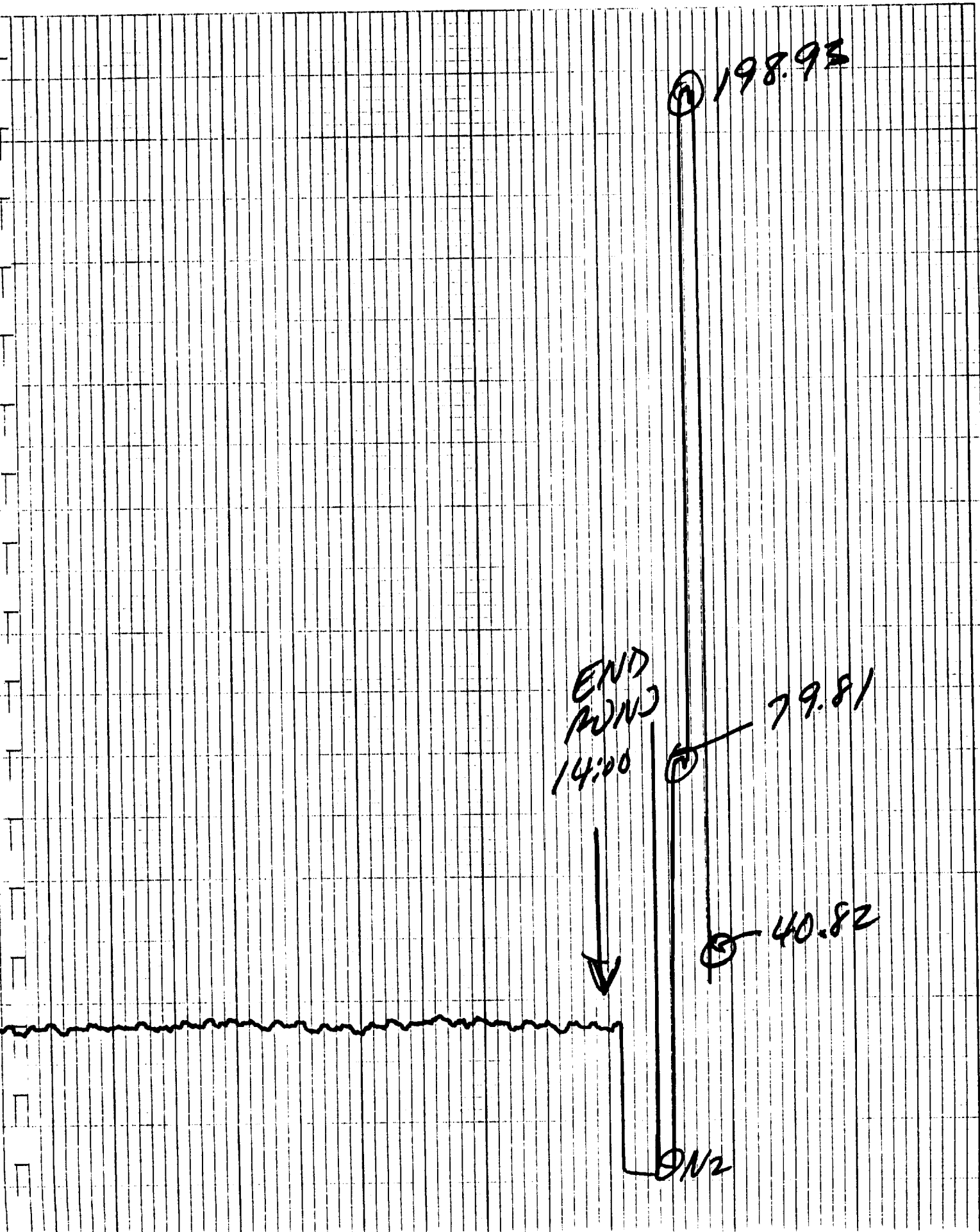




START  
RUN 2  
11:00







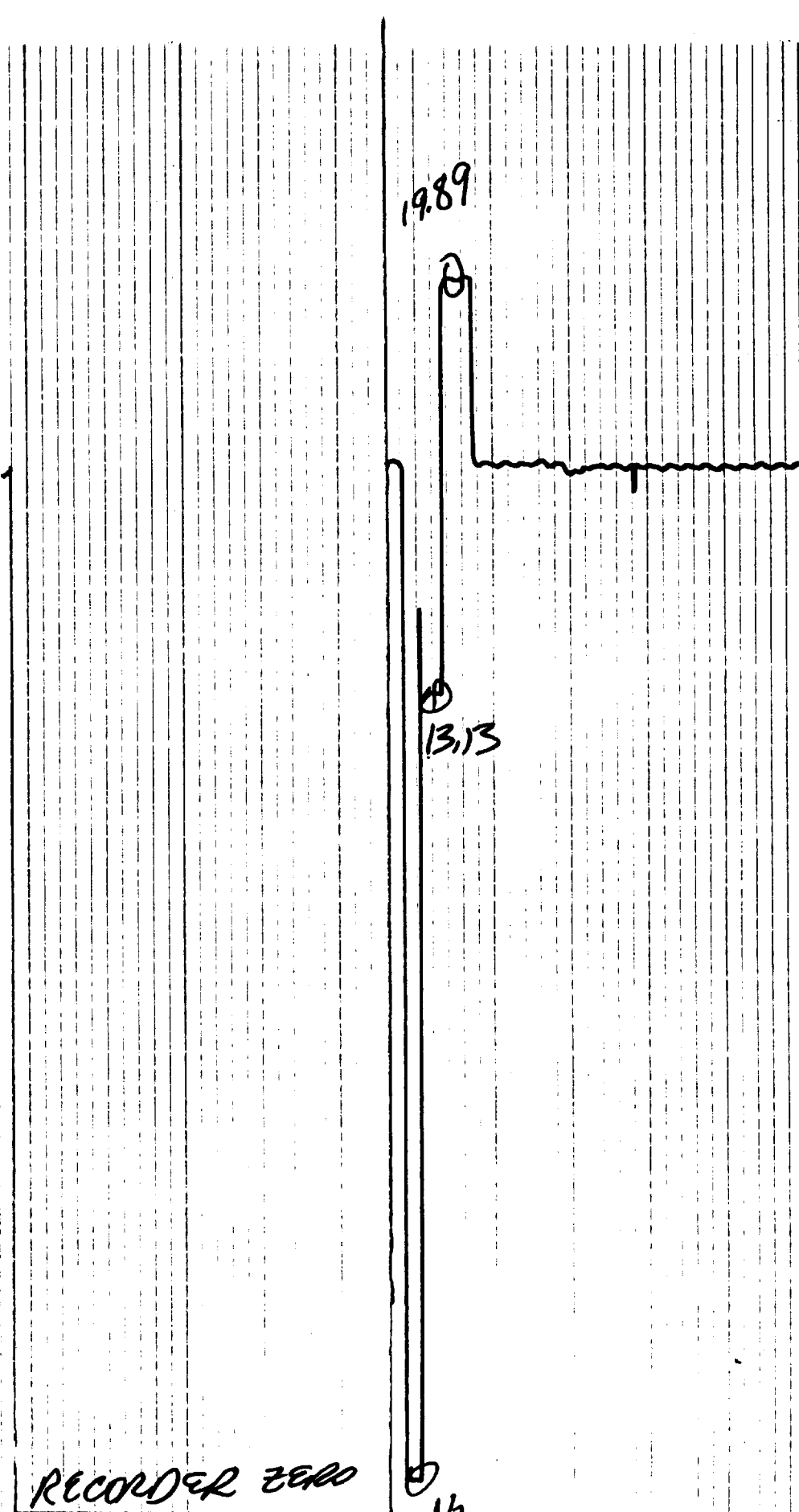


ANODIC  
REDUCTION

6/27/88

OXYGEN

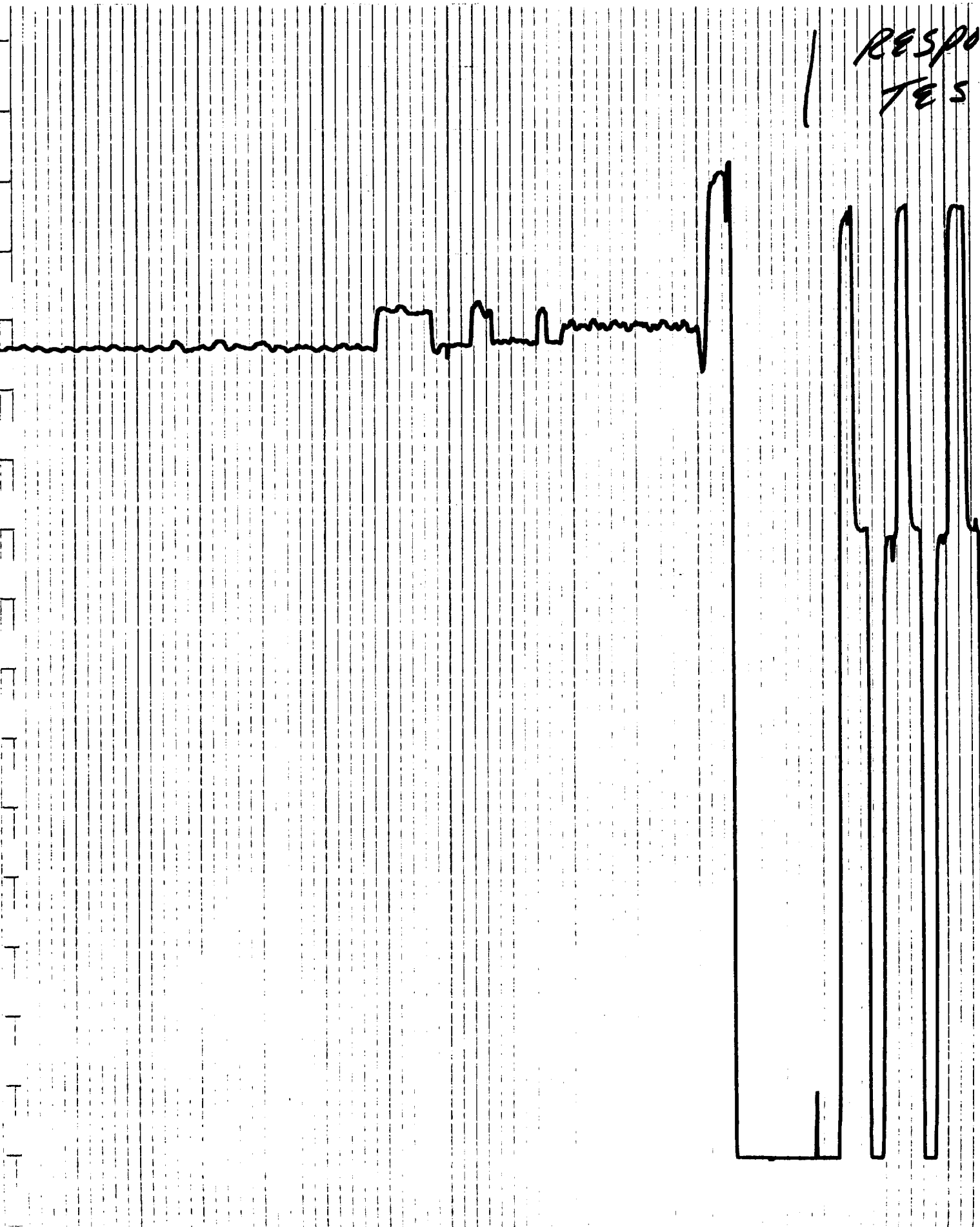
SETUP  
MORNING

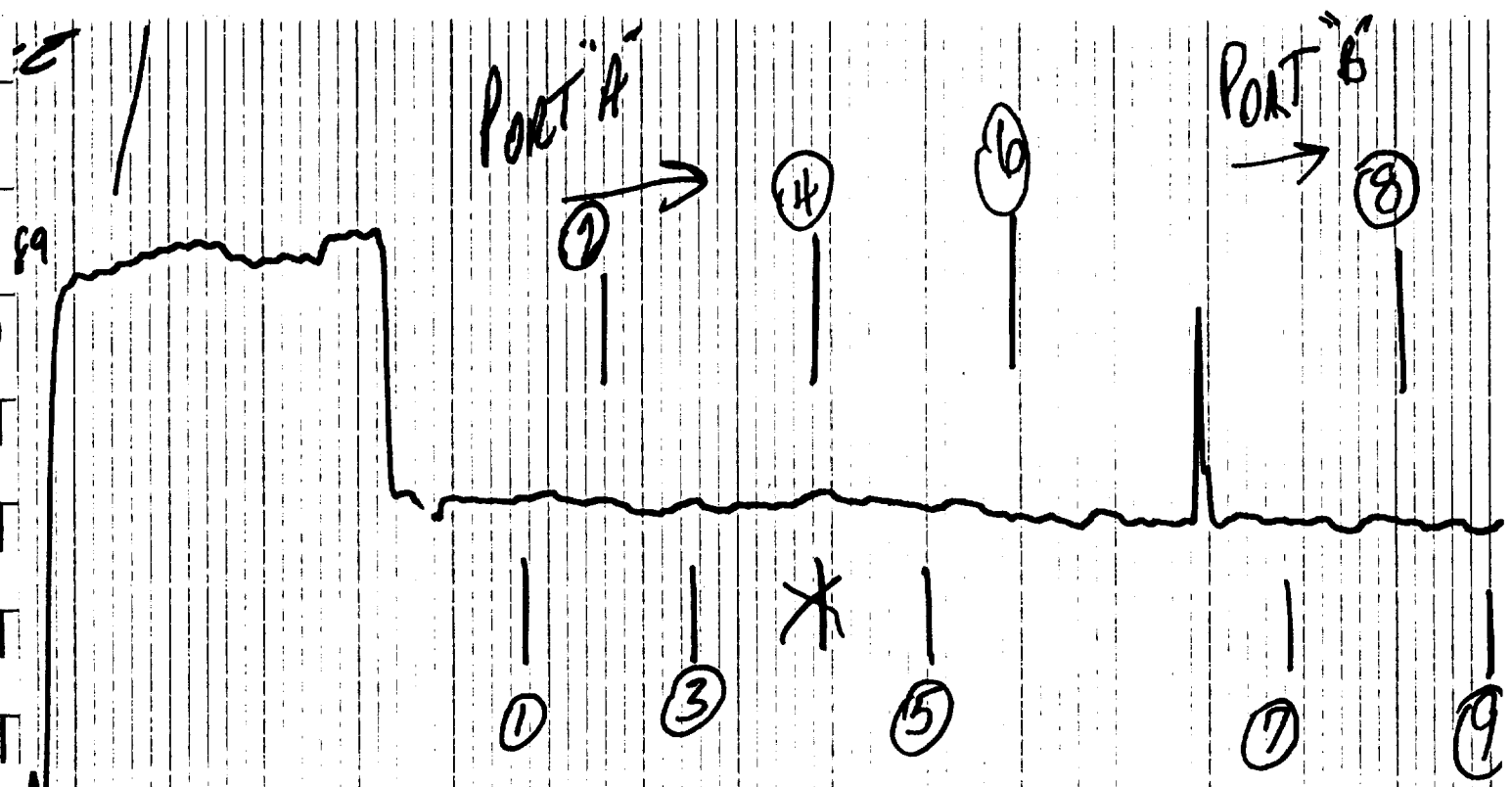


RECORDER ZERO

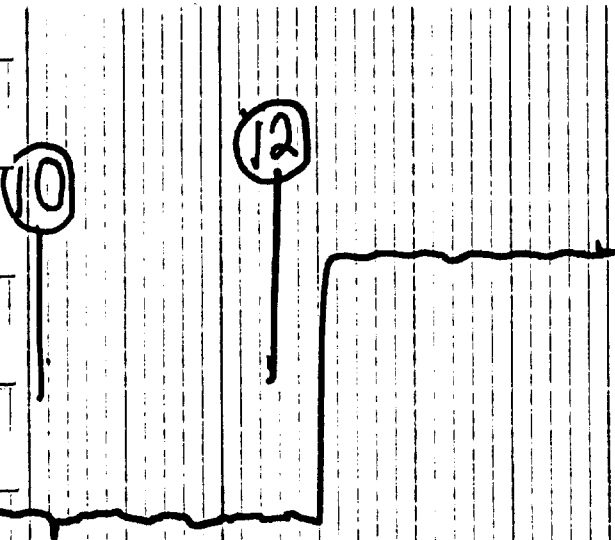
0  
N<sub>2</sub>

RESPO  
TES





OXYGEN TRAVERSE



11

Amoco  
Production

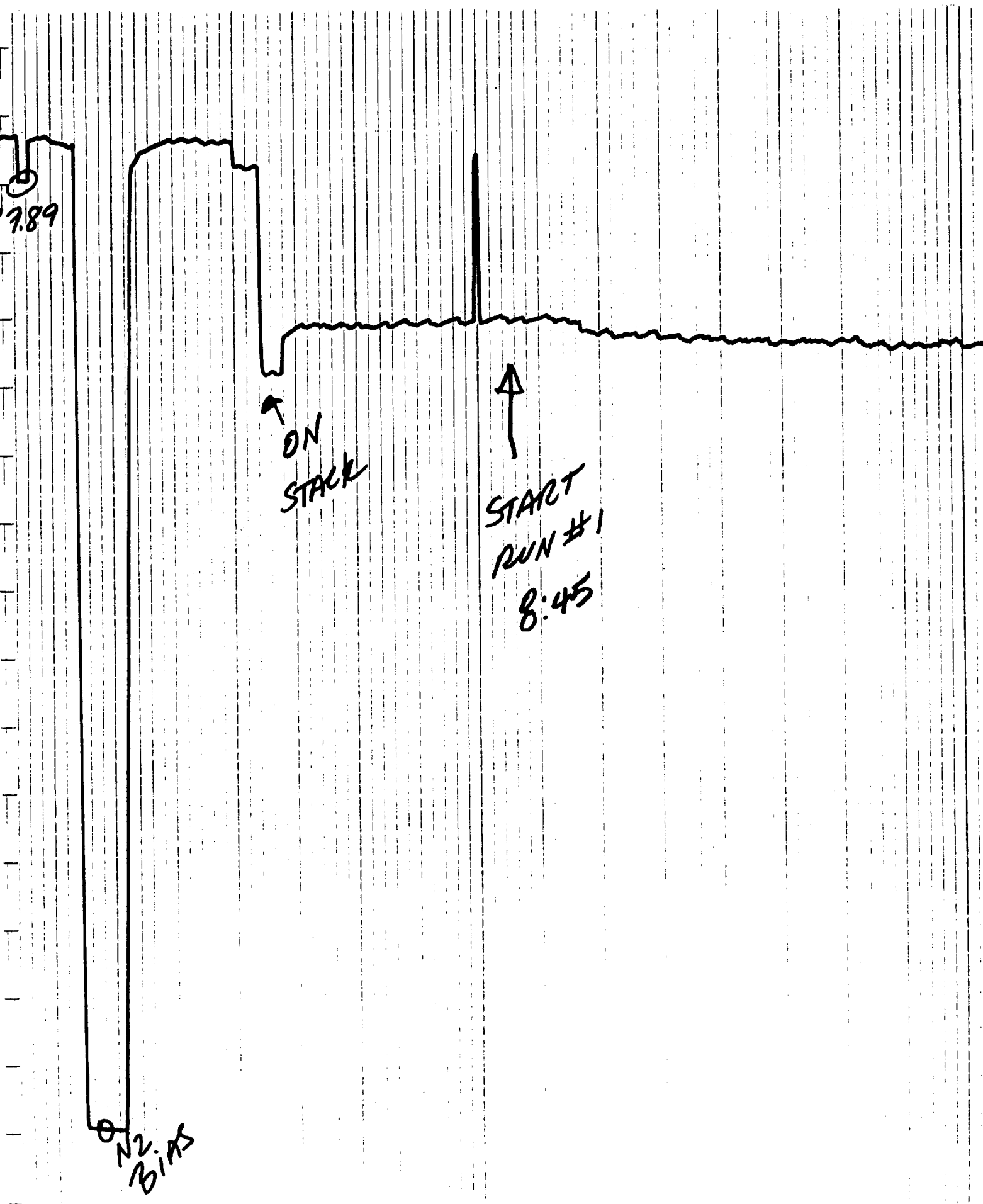
Oxygen

6/28/88



13.

N2

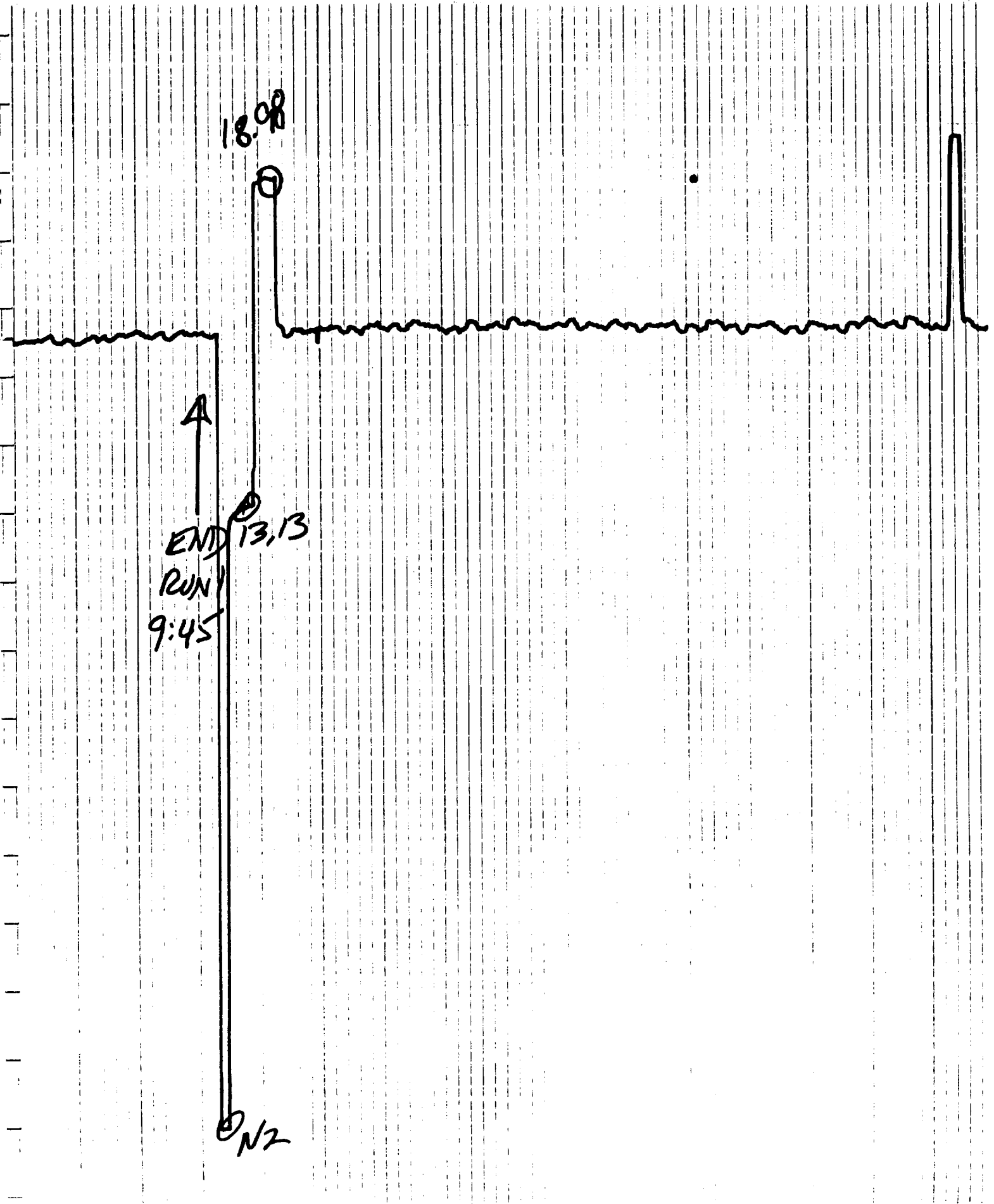


7.89

ON  
STACK

START  
RUN #1  
8:45

N2  
BIAS



18.08

0

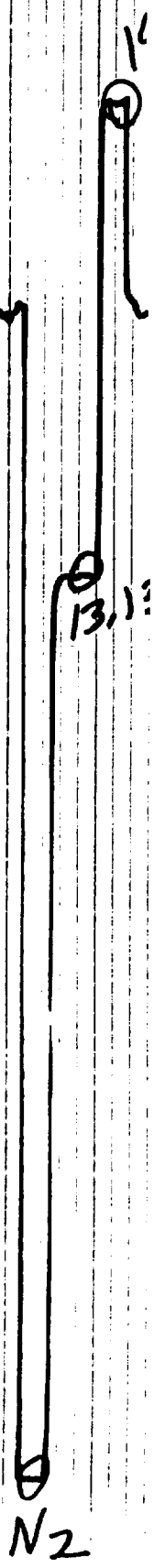
A

END 13.13  
RUNY  
9:45

0  
N2

START  
RUN #2  
11:00

END  
RUN #2  
12:00

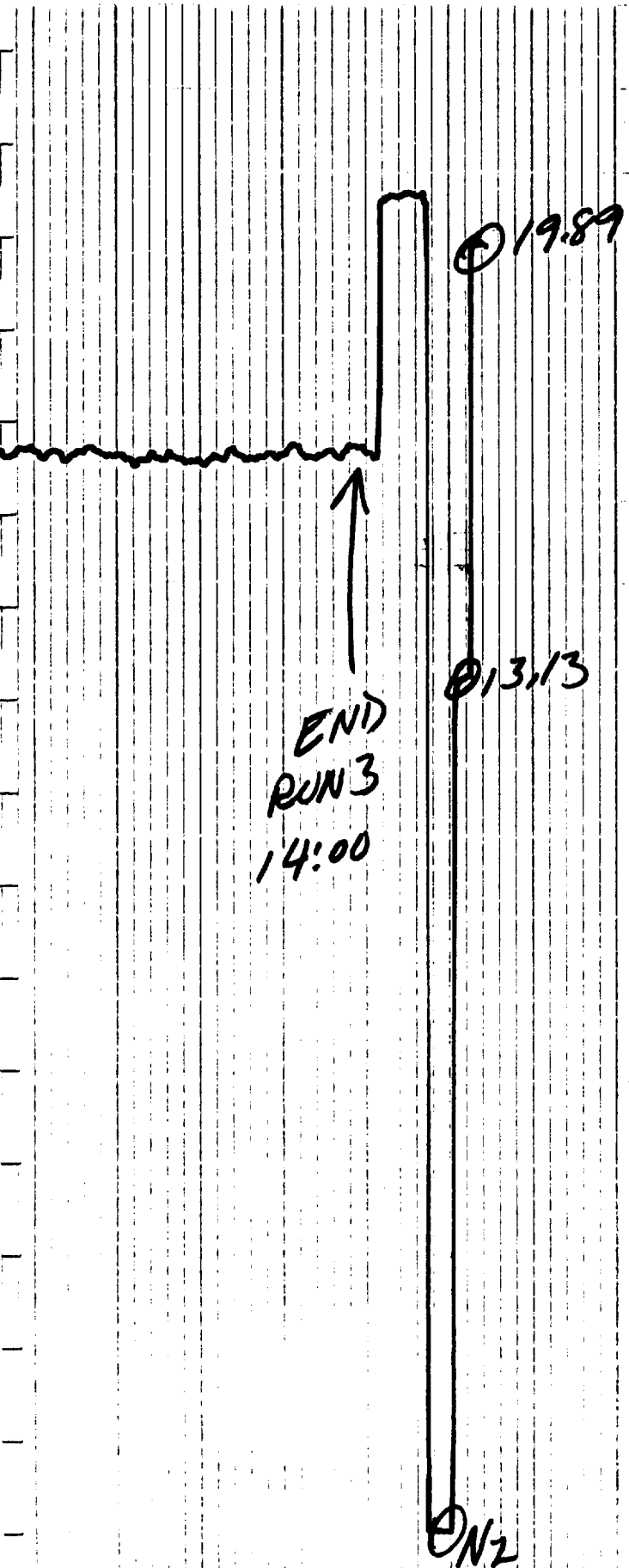


59



START  
RUN #2  
13:00





TURBINE OPERATIONAL RECORD

Company Name AMOCO PRODUCTION COMPANY  
Company Location MORGANZA SWT. PLT.  
Turbine Name SATURN (SINGLE SHAFT)  
Turbine Source I. D. No. 87-4

Design Specifications

Manufacturer's Name SOLAR TURBINES INCORPORATED  
Model No. GC1-5B-KATO  
Serial No. SG 87917

Parameter Specifications

- A. Fuel Type NATURAL GAS      B. Fuel Supplier AMOCO
- C. Fuel Flow Units MMCFD      Meas. Method ORFICE PLATE & METER
- D. Is unit equipped for waste heat recovery? YES  
Describe THERMO-FLOOD
- E. Does unit use water or steam injection? NO  
Describe measurement method (continuous flow, start-finish volumes, etc) N/A
- F. Combustor Inlet Pressure units (psia, kpa, etc.) 67 PSI
- G. Combustor Inlet Temperature units N/A

Ultimate Fuel Analysis

C \_\_\_\_\_ S \_\_\_\_\_ H \_\_\_\_\_ Ash \_\_\_\_\_  
O \_\_\_\_\_ H<sub>2</sub>O \_\_\_\_\_ N \_\_\_\_\_

Trace Metals: Na \_\_\_\_\_ Va \_\_\_\_\_ K \_\_\_\_\_

Fuel elements added \_\_\_\_\_

Fuel elements added for smoke suppression \_\_\_\_\_

TURBINE TEST RUN LOG 1st run

Turbine Operator Daniel K Dandy

Date 6-28-88 Time: Start 0835 End 0935

Ambient Temperature, at time of test 97°F

Turbine Load Condition % 100%

DATA LOG TIME (15 minute intervals)	<u>0835</u>	<u>0850</u>	<u>0905</u>	<u>0920</u>
Fuel Feed (flow) MCFD	<u>281</u>	<u>281</u>	<u>278</u>	<u>278</u>
<del>Steam to Turbine (flow)</del>	<u>    </u>	<u>    </u>	<u>    </u>	<u>    </u>
<del>Exhaust Temp</del>	<u>    </u>	<u>    </u>	<u>    </u>	<u>    </u>
Turbine Speed (rpm)	<u>22,300</u>	<u>22,300</u>	<u>22,300</u>	<u>22,300</u>
Combustor Inlet Temperature	<u>N/A</u>	<u>N/A</u>	<u>N/A</u>	<u>N/A</u>
OK Combustor Inlet Pressure	<u>68 psi</u>	<u>68 psi</u>	<u>67 psi</u>	<u>67 psi</u>
Generator Load (Kw) / Temp Eff	<u>800 / 880°F</u>	<u>790 / 875°F</u>	<u>780 / 870</u>	<u>775 / 870</u>
Combustor Chamber Pressure	<u>N/A</u>	<u>N/A</u>	<u>N/A</u>	<u>N/A</u>

Run Conditions: \_\_\_\_\_  
\_\_\_\_\_  
\_\_\_\_\_

Remarks: \_\_\_\_\_  
\_\_\_\_\_  
\_\_\_\_\_

operator log

TURBINE TEST RUN LOG 16T run

Turbine Operator David K. Derly

Date 6-28-88 Time: Start 0935 End \_\_\_\_\_

Ambient Temperature, at time of test \_\_\_\_\_

Turbine Load Condition % 100%

DATA LOG TIME (15 minute intervals)	<u>0935</u>	<u>0950</u>	_____	_____
Fuel Feed (flow) MCFD	<u>278</u>	<u>278</u>	_____	_____
<del>Steam to Turbine (flow)</del>	_____	_____	_____	_____
<del>Exhaust Temp</del>	_____	_____	_____	_____
Turbine Speed (rpm)	<u>22,300</u>	_____	_____	_____
Combustor Inlet Temperature	<u>N/A</u>	<u>N/A</u>	_____	_____
Combustor Inlet Pressure	<u>67 psi</u>	<u>67</u>	_____	_____
Generator Load (Kw)/Engine Exh.	<u>780/775</u>	<u>745/765</u>	_____	_____
Combustor Chamber Pressure	<u>N/A</u>	<u>N/A</u>	_____	_____

Run Conditions: \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_

Remarks: \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_

operator log

TURBINE TEST RUN LOG 2nd run

Turbine Operator Daniel R. Denny

Date 6-28-88 Time: Start 1100 End 1200

Ambient Temperature, at time of test 102

Turbine Load Condition % 100%

DATA LOG TIME (15 minute intervals)	<u>1100</u>	<u>1115</u>	<u>1130</u>	<u>1145</u>
Fuel Feed (flow) MCFD	<u>260</u>	<u>260</u>	<u>260</u>	<u>260</u>
<del>Steam to Turbine (flow)</del>	<u>      </u>	<u>      </u>	<u>      </u>	<u>      </u>
<del>Exhaust Temp</del>	<u>      </u>	<u>      </u>	<u>      </u>	<u>      </u>
Turbine Speed (rpm)	<u>22,300</u>	<u>22,300</u>	<u>22,300</u>	<u>22,300</u>
Combustor Inlet Temperature	<u>N/A</u>	<u>N/A</u>	<u>N/A</u>	<u>N/A</u>
Combustor Inlet Pressure	<u>66psi</u>	<u>66psi</u>	<u>66psi</u>	<u>66psi</u>
Generator Load (Kw) / Exhaust Temp.	<u>740/870°F</u>	<u>750/880°F</u>	<u>750/870°F</u>	<u>750/880°F</u>
Combustor Chamber Pressure	<u>N/A</u>	<u>N/A</u>	<u>N/A</u>	<u>N/A</u>

Run Conditions: \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_

Remarks: \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_

operator log

TURBINE TEST RUN LOG 2nd Run

Turbine Operator Daniel R. Dendy

Date 6-28-88 Time: Start 1100 End 1200

Ambient Temperature, at time of test 102°F

Turbine Load Condition % 100%

DATA LOG TIME (15 minute intervals)	<u>1200</u>	_____	_____	_____
Fuel Feed (flow)	<u>260</u>	_____	_____	_____
<del>Steam to Turbine (flow)</del>	_____	_____	_____	_____
<del>ENGINE Exhaust Temp</del>	_____	_____	_____	_____
Turbine Speed (rpm)	<u>22,300</u>	_____	_____	_____
Combustor Inlet Temperature	<u>N/A</u>	_____	_____	_____
Combustor Inlet Pressure	<u>66 psi</u>	_____	_____	_____
Generator Load (Kw) / Exhaust Temp	<u>735 / 870°F</u>	_____	_____	_____
Combustor Chamber Pressure	<u>N/A</u>	_____	_____	_____

Run Conditions: \_\_\_\_\_  
\_\_\_\_\_  
\_\_\_\_\_

Remarks: \_\_\_\_\_  
\_\_\_\_\_  
\_\_\_\_\_

Operator Log

TURBINE TEST RUN LOG 3rd Run

Turbine Operator Daniel K. Dendy

Date 6-28-88 Time: Start 1200 End 1300

Ambient Temperature, at time of test 97°

Turbine Load Condition % 100%

DATA LOG TIME (15 minute intervals)	<u>1200</u>	<u>1215</u>	<u>1230</u>	<u>1245</u>
Fuel Feed (flow) MCFD	<u>260</u>	<u>260</u>	<u>260</u>	<u>260</u>
<del>Steam to Turbine (flow)</del>	<u>      </u>	<u>      </u>	<u>      </u>	<u>      </u>
<del>ENGINE Exhaust Temp</del>	<u>      </u>	<u>      </u>	<u>      </u>	<u>      </u>
Turbine Speed (rpm)	<u>22,300</u>	<u>22,300</u>	<u>22,300</u>	<u>22,300</u>
Combustor Inlet Temperature	<u>N/A</u>	<u>N/A</u>	<u>N/A</u>	<u>N/A</u>
Combustor Inlet Pressure	<u>66 psi</u>	<u>66 psi</u>	<u>66 psi</u>	<u>65 psi</u>
Generator Load (Kw) / Exhaust Temp.	<u>750/885</u>	<u>750/880</u>	<u>740/865</u>	<u>750/880</u>
Combustor Chamber Pressure	<u>N/A</u>	<u>N/A</u>	<u>N/A</u>	<u>N/A</u>

Run Conditions: \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_

Remarks: \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_

Operator Log

TURBINE TEST RUN LOG

3rd run

Turbine Operator Daniel R. Dandy

Date 6-28-88 Time: Start 1300 End \_\_\_\_\_

Ambient Temperature, at time of test 97°

Turbine Load Condition % 100%

DATA LOG TIME	<u>1300</u>	_____	_____	_____
(15 minute intervals)				
Fuel Feed (flow) MCFD	<u>260</u>	_____	_____	_____
<del>Steam to Turbine (flow)</del>	_____	_____	_____	_____
<del>ENGINE Exhaust Temp</del>	_____	_____	_____	_____
Turbine Speed (rpm)	<u>22,300</u>	_____	_____	_____
Combustor Inlet Temperature	<u>N/A</u>	_____	_____	_____
Combustor Inlet Pressure	<u>65</u>	_____	_____	_____
Generator Load (Kw) / Exhaust Temp	<u>740/850</u>	_____	_____	_____
Combustor Chamber Pressure	<u>N/A</u>	_____	_____	_____

Run Conditions: \_\_\_\_\_

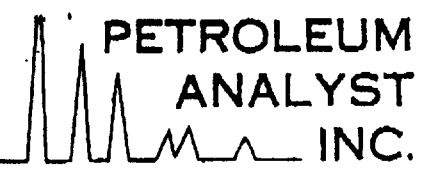
\_\_\_\_\_

Remarks: \_\_\_\_\_

\_\_\_\_\_

operator log





**PETROLEUM  
ANALYST  
INC.**

**ANALYTICAL CONSULTANTS**

GAS ANALYSIS REPORT NO: 013-062988-01      DATE: 06-29-88

OR: AMOCO PRODUCTION COMPANY      SAMPLE IDENTIFICATION:  
 ATTN: GAS MEAS. SEC.      COMPANY: AMOCO PRODUCTION      JB  
 P.O. BOX 39500      FIELD: MORGANZA CF#1 40-665  
 LAFAYETTE LA 70593      LEASE: TURBINE FUEL

SAMPLE DATA:      DATE: 06-28-88      BY: J. BENDILY  
 PSIG: 146      TEMP: 106 DEG.F.      GRAV: .612  
 MCF/D: 250      DIF: 34 IN.      DP: LBS H2O

REMARKS: H2S (FIELD TEST) = 2.5 PPM  
 TIME 9:05 AM

CYL # 413

**COMPONENT ANALYSIS**

COMPONENT	MOL PERCENT	GPM @ 15.025 PSIA
CARBON DIOXIDE (CO2)	1.30	
NITROGEN (N2)	0.18	
METHANE (C1)	92.79	
ETHANE (C2)	3.67	1.001
PROPANE (C3)	0.80	0.225
ISO-BUTANE (IC4)	0.25	0.083
N-BUTANE (NC4)	0.20	0.064
ISO-PENTANE (IC5)	0.13	0.049
N-PENTANE (NC5)	0.07	0.026
HEXANES (C6)	0.17	0.071
HEPTANES PLUS (C7+)	0.44	0.207
<b>TOTAL</b>	<b>100.00</b>	
	ETHANE + GPM	1.726
	ISO-PENTANE + GPM	0.353
	<b>COMPRESSIBILITY FACTOR</b>	<b>0.9975</b>
	<b>SPECIFIC GRAVITY @ 60 DEG. F. (AIR = 1)</b>	<b>0.622</b>
<b>BTU/CU. FT. @ 60 DEG. F.. 15.025 PSIA</b>	<b>DRY</b>	<b>1104.1</b>
	<b>WET</b>	<b>1085.3</b>

9



**PETROLEUM  
ANALYST  
INC.**

**ANALYTICAL CONSULTANTS**

**GAS ANALYSIS REPORT NO: 014-062988-01      DATE: 06-29-88**

**FOR: AMOCO PRODUCTION COMPANY  
ATTN: GAS MEAS. SEC.  
P.O. BOX 39500  
LAFAYETTE LA 70593**

**SAMPLE IDENTIFICATION:  
COMPANY: AMOCO PRODUCTION      JB  
FIELD: MORGANZA CF#1 40-665  
LEASE: TURBINE FUEL**

**SAMPLE DATA:      DATE: 06-28-88      BY: J. BENDILY  
PSIG: 147      TEMP: 116 DEG.F.      GRAV: .618  
MCF/D: 250      DIF: 33 IN.      DP:      LBS H2O**

**REMARKS: H2S (FIELD TEST) = 2.5 PPM  
TIME 11:20 AM**

**CYL. # 310**

**COMPONENT ANALYSIS**

COMPONENT	MOL PERCENT	GFM @ 15.025 PSIA
CARBON DIOXIDE (CO2)	1.37	
NITROGEN (N2)	0.15	
METHANE (C1)	92.97	
ETHANE (C2)	3.64	0.993
PROPANE (C3)	0.78	0.219
ISO-BUTANE (IC4)	0.23	0.077
N-BUTANE (NC4)	0.16	0.051
ISO-PENTANE (IC5)	0.13	0.049
N-PENTANE (NC5)	0.07	0.026
HEXANES (C6)	0.15	0.063
HEPTANES PLUS (C7+)	0.35	0.165
<b>TOTAL</b>	<b>100.00</b>	
	ETHANE + GFM	1.643
	ISO-PENTANE + GFM	0.303
	<b>COMPRESSIBILITY FACTOR</b>	<b>0.9975</b>
	<b>SPECIFIC GRAVITY @ 60 DEG. F. (AIR = 1)</b>	<b>0.618</b>
<b>BTU/CU. FT. @ 60 DEG. F., 15.025 PSIA</b>	<b>DRY</b>	<b>1096.8</b>
	<b>WET</b>	<b>1078.1</b>

PETROLEUM ANALYST INC.

ANALYTICAL CONSULTANTS

GAS ANALYSIS REPORT NO: 015-062988-01 DATE: 06-29-88

FOR: AMOCO PRODUCTION COMPANY
ATTN: GAS MEAS. SEC.
P.O. BOX 39500
LAFAYETTE LA 70593

SAMPLE IDENTIFICATION:
COMPANY: AMOCO PRODUCTION JB
FIELD: MORGANZA CF#1 40-665
LEASE: TURBINE FUEL

SAMPLE DATA: DATE: 06-28-88 BY: J. BENDILY
PSIG: 148 TEMP: 108 DEG.F. GRAV: .615
MCF/D: 250 DIF: 35 IN. DP: LBS H2O

REMARKS: H2S (FIELD TEST) = 2.5 PPM
TIME 1:30 PM

CYL # 208

COMPONENT ANALYSIS

Table with 3 columns: COMPONENT, MOL PERCENT, GPM @ 15.025 PSIA. Rows include CARBON DIOXIDE, NITROGEN, METHANE, ETHANE, PROPANE, ISO-BUTANE, N-BUTANE, ISO-PENTANE, N-PENTANE, HEXANES, HEPTANES PLUS.

TOTAL 100.00

ETHANE + GPM 1.671
ISO-PENTANE + GPM 0.331

COMPRESSIBILITY FACTOR 0.9975

SPECIFIC GRAVITY @ 60 DEG. F. (AIR = 1) 0.620

BTU/CU. FT. @ 60 DEG. F., 15.025 PSIA DRY 1099.5
WET 1080.8

## VII. APPENDIX

Contained in this section are the dry gas meter calibration, wet test meter calibration, pitot tube calibration, gas standard certifications and resumes of the persons performing the testing. Also included are excerpts from the instrument operations manuals for all analytical instruments used, showing the principle of operation, performance specifications, flow diagrams, etc..

John R. Angelloz, Jr.  
Sampling Specialist  
ETS Incorporated  
Baton Rouge, Louisiana

#### EDUCATION

B.S., Engineering Technology  
Louisiana State University

Engineer Officer Advanced Course, 1988  
Fort Belvoir, Virginia

Engineer Officer Basic Course, 1983  
Fort Belvoir, Virginia

#### EXPERIENCE

1984 to Present - Transferred to ETS from Kemron when ETS purchased assets. Testing Team Leader experienced in emission testing, fugitive emissions, continuous emissions and ambient air monitoring. Familiar with all routine US EPA New Source Performance Test procedures. Routinely performs source sampling and testing using Reference Method test as well as non-standard testing procedures. Conducts calibration, repair and routine maintenance of source sampling and continuous emission monitoring equipment. Responsible for equipment and crew preparation, calibration and logistics for sampling and testing projects.

1984 - Ashton and Associates - Computer Plotter Operator for engineering drawings and prints. Responsible for current materials inventory control.

1975 to 1984 - St. Alphonsus Church. Maintenance Supervisor of maintenance personnel. Responsible for scheduling work, ordering materials, quality control, maintenance safety, and time motion sequences.

#### MILITARY

Louisiana National Guard - CPT. - Active duty

Troy W. LeSage  
Sampling Specialist  
ETS Incorporated  
Baton Rouge, Louisiana

#### EDUCATION

Central High School

#### EXPERIENCE

1987 to Present - Emission testing specialist for ETS.  
Performs EPA reference methods for compliance testing as well as other non-routine source evaluations. Responsibilities also include job preparation, equipment calibration, and equipment maintenance.

1985 to 1987 - Industrial Hygiene Technican for an environmental firm, performing metal analysis with atomic adsorption spectrophotometer, fiber analysis for asbestos and overseeing asbestos abatement projects.

EPA - Sampling and evaluation of Airborn Asbestos Temple University

Air pollution control orientation course

Certified Emissions Opacity Reader.

Niosh - Supervision of Asbestos Abatement Projects, Texas A&M

Steven J. Schwartz  
Instrumentation Engineer  
ETS Incorporated  
Baton Rouge, Louisiana

#### EDUCATION

- A.A., Engineering  
Palm Beach Junior College
- B.S., Chemical Engineering  
University of Southwestern Louisiana
- B.S., Chemistry  
University of Southwestern Louisiana

#### EXPERIENCE

1987 to present - Emission Testing Services, Inc. Field testing of stack gases and parameters governing the performance of stationary sources. Knowledgeable with the EPA Reference Methods 1-11, 20 and 25A compliance tests and analysis.

1985 to 1987 - University of Southwestern Louisiana. Student stockroom assistant. Responsibilities include the standardization and quality control of all research and classroom reagents and chemicals. Coordinated the calibration and maintenance of laboratory instruments and analyzers.

1982 to 1985 - Service Lab Analysis, Inc., Laboratory Manager. Involved in all phases of wastewater, ground water and soil analysis as proposed by the Louisiana Department of Natural Resources, 29-B. Detailed laboratory investigations of EPA methodology analysis of pesticides, organic and inorganic matter according to SW-846. Group leader and oversaw the proposals and technical reports to clients.

METER BOX CALIBRATION DATA AND CALCULATION FORM

(English Units)

Date 4-7-88

Meter box number 586

Barometric pressure,  $P_b$  30.82 in. Hg

Calibrated by Troy LePage

Orifice manometer setting ( $\Delta H$ ), in. H <sub>2</sub> O	Wet test meter ( $V_w$ ), ft <sup>3</sup>	Dry gas meter ( $V_d$ ), ft <sup>3</sup>	Wet test meter ( $t_w$ ), °F	Dry gas meter			Time (O), min.
				Inlet ( $t_{d_i}$ ), °F	Outlet ( $t_{d_o}$ ), °F	Avg <sup>a</sup> ( $t_d$ ), °F	
0.5	5	812.000	63°	75 79	72 74		12.97
1.0	5	816.963	64°	79 83	74 76		9.24
1.5	10	821.917	65°	82 86	75 78		15.25
2.0	10	831.8 <sup>05</sup>	65°	84 90	77 79		12.16
3.0	10	841.676	66°	88 93	78 82		11.05
4.0	10	851.549					

$\Delta H$ , in. H <sub>2</sub> O	$\frac{\Delta H}{13.6}$	$Y_i = \frac{V_w P_b (t_d + 460)}{V_d (P_b + \frac{\Delta H}{13.6}) (t_w + 460)}$	$\Delta H @_i = \frac{0.0317 H}{P_b (t_d + 460)} \left[ \frac{(t_w + 460) O}{V_w} \right]^2$
0.5	0.0368	1.029	1.763
1.0	0.0737	1.034	1.783
1.5	0.110	1.037	1.818
2.0	0.147	1.042	1.963
3.0	0.221	1.042	1.894
4.0	0.294		
Average		1.037	1.844

$Y$  = Ratio of reading of wet test meter to dry test meter; tolerance for individual values + 0.02 from average.

$H @$  = Orifice pressure differential that equates to 0.75 cfm of air @ 68 F and 29.92 inches of mercury, in. H<sub>2</sub>O; tolerance for individual values + 0.20 from average.

Calibrated by Troy S. Dool



Wet test meter serial number P-1388 Date 03-04-88

Range of wet test meter flow rate 0-50 ft<sup>3</sup>/hr  
Volume of test flask  $V_s =$  0.20 ft<sup>3</sup>/hr wet test meter

Satisfactory leak check? Yes  
Ambient temperature of equilibrate liquid in wet test meter and reservoir 77.8°F

Test number	Manometer reading, mm H <sub>2</sub> O	Final volume (V <sub>f</sub> ), ℓ	Initial volume (V <sub>i</sub> ), ℓ	Total volume (V <sub>m</sub> ) <sup>b</sup> , ℓ	Flask volume (V <sub>s</sub> ), ℓ	Percent error, %
1	0.01	282.9035	0.0	282.9035	283.1017	-0.001
2	0.01	565.9535	282.9035	283.0500	286.0277	-0.010
3	0.01	849.5430	565.9535	283.5895	287.8433	-0.015

<sup>a</sup> Must be less than 10 mm (0.4 in.) H<sub>2</sub>O.

Calculations:

<sup>b</sup>  $V_m = V_f - V_i$ .

<sup>c</sup> % error =  $100 (V_m - V_s) / V_s =$  -0.009 (+1%).

Sean J. [Signature] Signature of calibration person

Wet test meter calibration log.

PITOT TUBE CALIBRATION

Pitot Tube Number P-3-3

Cp (std) 0.99

Calibrated By T. LeSage

Date 2-2-88

Point Number	Standard Pitot Δ p (in. H <sub>2</sub> O)	"S" Type Pitot Δ p (in. H <sub>2</sub> O)	
		"A" Side	"B" Side
1	<u>0.110</u>	<u>0.170</u>	<u>0.170</u>
2	<u>0.545</u>	<u>0.820</u>	<u>0.815</u>
3	<u>0.845</u>	<u>1.35</u>	<u>1.30</u>

Calculations:

$$Cp_{(s)} = Cp_{(std)} \times \sqrt{\frac{\Delta p (std)}{\Delta p (s)}}$$

Deviation =  $Cp_{(s)} - \bar{Cp}$  (Side A or B)

Avg. Dev. =  $\frac{\sum |Cp_{(s)} - \bar{Cp}|}{3}$  (Side A or B)

"A" Side		"B" Side	
Cp(s)	Deviation	Cp(s)	Deviation
<u>0.796</u>	<u>0.003</u>	<u>0.796</u>	<u>0.005</u>
<u>0.807</u>	<u>0.008</u>	<u>0.810</u>	<u>0.009</u>
<u>0.783</u>	<u>0.016</u>	<u>0.798</u>	<u>0.003</u>

$\bar{Cp} = \underline{0.799}$  =  $\underline{0.801}$

$|\bar{Cp} (Side A) - \bar{Cp} (Side B)| = \underline{0.002}$  (must be  $\leq 0.01$ )

Avg. Dev. (Side A) =  $\underline{0.009}$  (must be  $\leq 0.01$ )

(Side B) =  $\underline{0.006}$  (must be  $\leq 0.01$ )

$Cp = \frac{\bar{Cp} (Side A) + \bar{Cp} (Side B)}{2}$  (should be  $0.80 \leq Cp \leq 0.85$ ) =  $\underline{0.80}$

Date Shipped 10/23/87  
 Our Project No: 924300  
 Your P.O. No: VERBAL  
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## CERTIFICATE OF ANALYSIS - EPA PROTOCOL GASES\*

(Concentrations are in mole % or ppm)

Cylinder Number AAL-4812 Certified Accuracy ±1% % NBS Traceable Analysis Dates: First 10/12/87 Last 10/21/87

P-0783 CYLINDER PRESSURE 1900 PSIG

COMPONENTS	CERTIFIED CONC	EXPIRATION DATE	ANALYTICAL PRINCIPLE	PRIMARY STANDARD NBS/SRM'S	REPLICATE CONCENTRATIONS	
					FIRST	SECOND
NITRIC OXIDE	197.08 PPM	3/21/89	HORIBA CHEMILUMINESCENCE		196.20 PPM	197.32 PPM
NITROGEN DIOXIDE	1.85 PPM (NOT PROTOCOLED)			1687 B CAL-9063 951 PPM	197.95 PPM	196.97 PPM
NITROGEN	BALANCE			1658B 243 PPM FF-19356	197.95 PPM	196.97 PPM

Cylinder Number      Certified Accuracy      % NBS Traceable Analysis Dates: First      Last     

COMPONENTS	CERTIFIED CONC	EXPIRATION DATE	ANALYTICAL PRINCIPLE	PRIMARY STANDARD NBS/SRM'S	REPLICATE CONCENTRATIONS	
					FIRST	SECOND

\*We hereby certify the cylinder gas has been analyzed according to EPA Protocol No:

Analyst *Patricia K. Kamin* Approved By *J. Shapiro*

The only liability of this Company for gas which fails to comply with this analysis shall be replacement thereof by the Company without extra cost.

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Date Shipped 10/23/87

Our Project No: 924-300

Your P.O. No: VERBAL

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## CERTIFICATE OF ANALYSIS - EPA PROTOCOL GASES\*

(Concentrations are in mole % or ppm)

Cylinder Number AAL-13230 Certified Accuracy ±1% % NBS Traceable Analysis Dates: First 10/12/87 Last 10/22/87

P-0787 CYLINDER PRESSURE 2200 PSIG

COMPONENTS	CERTIFIED CONC	EXPIRATION DATE	ANALYTICAL PRINCIPLE	PRIMARY STANDARD NBS/SRM's	REPLICATE CONCENTRATIONS	
					FIRST	SECOND
NITRIC OXIDE	77.30 PPM	3/21/89	HORIBA	1684B FF24138	76.87 PPM	77.20 PPM
NITROGEN DIOXIDE	2.51 PPM (NOT PROTOCOLED)		CHEMILUMINESCENCE	93.7 PPM	77.43 PPM	77.10 PPM
NITROGEN	BALANCE			1638B FF26385	77.33 PPM	77.60 PPM
				49.5 PPM		

Cylinder Number                      Certified Accuracy            % NBS Traceable Analysis Dates: First            Last           

COMPONENTS	CERTIFIED CONC	EXPIRATION DATE	ANALYTICAL PRINCIPLE	PRIMARY STANDARD NBS/SRM's	REPLICATE CONCENTRATIONS	
					FIRST	SECOND

\*We hereby certify the cylinder gas has been analyzed according to EPA Protocol No:                     

Analyst *F. Shapiro* Approved By *F. Shapiro*

The only liability of this Company for gas which fails to comply with this analysis shall be replacement thereof by the Company without extra cost.

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Date Shipped 10/23/87

Our Project No: 924300

Your P.O. No: VERBAL

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Cylinder Number AAL-2683

Certified Accuracy ±1% % NBS Traceable

Analysis Dates: First 10/12/87 Last 10/22/87

### CERTIFICATE OF ANALYSIS — EPA PROTOCOL GASES\*

(Concentrations are in mole % or ppm)

P-0786 CYLINDER PRESSURE 2200 PSIG

COMPONENTS	CERTIFIED CONC	EXPIRATION DATE	ANALYTICAL PRINCIPLE	PRIMARY STANDARD NBS/SRM's	REPLICATE CONCENTRATIONS	
					FIRST	SECOND
NITRIC OXIDE	40.32 PPM	3/21/89	HORIBA	FF24138	40.39 PPM	40.32 PPM
NITROGEN DIOXIDE	0.50 PPM (NOT PROTOOLED)		CHEMILUMINESCENCE	93.7 PPM	40.63 PPM	40.22 PPM
NITROGEN	BALANCE			FF26385	40.73 PPM	40.42 PPM
				49.5 PPM		

Cylinder Number                      Certified Accuracy            % NBS Traceable Analysis Dates: First            Last           

COMPONENTS	CERTIFIED CONC	EXPIRATION DATE	ANALYTICAL PRINCIPLE	PRIMARY STANDARD NBS/SRM's	REPLICATE CONCENTRATIONS	
					FIRST	SECOND

\*We hereby certify the            cylinder gas has been analyzed according to EPA Protocol No:           

Analyst *[Signature]* Approved By *[Signature]*

The only liability of this Company for gas which fails to comply with this analysis shall be replacement thereof by the Company without extra cost.

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**CERTIFICATE OF ANALYSIS - EPA PROTOCOL GASES\***  
 (Concentrations are in mole % or ppm)

Cylinder Number AAL-18938    Certified Accuracy 1 % NBS Traceable    Analysis Dates: First 8/21/87 Last 8/31/87

CYLINDER PRESSURE 2000 PSIG	COMPONENTS	CERTIFIED CONC	EXPIRATION DATE	ANALYTICAL PRINCIPLE	PRIMARY STANDARD NBS/SRM's	REPLICATE CONCENTRATIONS	
						FIRST	SECOND
	Carbon Monoxide	89.85 ppm	2/28/89	Beckman NDIR	1680B	89.58 ppm	89.99 ppm
	Nitrogen	Balance			CAL2284 475 ppm 1679C	89.99 ppm 89.58 ppm	89.58 ppm 89.99 ppm
					CAL5168 97.10 ppm		

Cylinder Number AAL-7912    Certified Accuracy 1 % NBS Traceable    Analysis Dates: First 8/24/87 Last 8/31/87

CYLINDER PRESSURE 2000 PSIG	COMPONENTS	CERTIFIED CONC	EXPIRATION DATE	ANALYTICAL PRINCIPLE	PRIMARY STANDARD NBS/SRM's	REPLICATE CONCENTRATIONS	
						FIRST	SECOND
	Carbon Monoxide	59.76 ppm	2/28/89	Beckman NDIR	1680B	60.16 ppm	59.76 ppm
	Nitrogen	Balance			CAL2284 475 ppm 1679C	60.16 ppm 60.16 ppm	59.76 ppm 59.76 ppm
					CAL5168 97.10 ppm		

\*We hereby certify the cylinder gas has been analyzed according to EPA Protocol No:

Analyst Bert Pappalardo    Approved By J. Shapiro

The only liability of this company for gas which fails to comply with this analysis shall be replacement thereof by the company without extra cost.

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# Scott Specialty Gases

a division of  
Scott Environmental Technology, Inc.

PLUMSTEADVILLE, PA 18949    PHONE: 215-766-8861    TWX: 510-565-9344

Shipped From: Scott

Date Shipped: 10/30/87

Our Project No.: 924300

Your P.O. No.: VERBAL

Page 1 of 1

Expiration Date: 4/29/89

Certified For Traceability Protocol No. 1 Procedure No. \_\_\_\_\_ Cylinder No. AAL-16677 Cylinder Pressure 1900 psig Certified Accuracy 1 % NBS Traceable

### CERTIFICATE OF ANALYSIS -- EPA PROTOCOL GASES\*

**PO 300**

COMPONENTS	CERTIFIED CONC	SRM/CRM NO.	CYL. NO.	CONC.	MAKE/MODEL/SERIAL NO.	LAST CAL. DATE	ANALYTICAL PRINCIPLE
CARBON MONOXIDE	29.34 PPM	1678C	FF-19750	45.60 PPM	HORIBA	10/23/87	NDIR
		1677	AAL-7314	9.90 PPM			

### REFERENCE STD

COMPONENTS	CERTIFIED CONC	SRM/CRM NO.	CYL. NO.	CONC.
CARBON MONOXIDE	29.34 PPM	1678C	FF-19750	45.60 PPM
		1677	AAL-7314	9.90 PPM

### BALANCE GAS : NITROGEN

### ANALYZER READINGS: Z = Zero Gas T = Test Gas R = Reference Gas

Component CARBON MONOXIDE

First Analysis Date 10/23/87 Units Milli-Volts

Z	0	R	98.4	T	58.3
R	98.5	Z	0	T	58.0
Z	0	T	58.0	R	98.5
		Mean Test Assay	29.39 PPM		

Second Analysis Date 10/29/87 Units Milli-Volts

Z	0	R	98.4	T	58.0
R	98.4	Z	0	T	58.0
Z	0	T	57.9	R	98.4
		Mean Test Assay	29.34 PPM		

Chronology: Date 10/29/87  
Assay 29.34 PPM

Component \_\_\_\_\_

Date	_____	Units	_____
Z	_____	R	_____
R	_____	Z	_____
Z	_____	T	_____
		Mean Test Assay	_____

Date \_\_\_\_\_

Z	_____	R	_____	T	_____
R	_____	Z	_____	T	_____
Z	_____	T	_____	R	_____
		Mean Test Assay	_____		

Analyst Bob Pentz

Approved By: J. Shapiro

Cylinder Number AAL-16113 Certified Accuracy ±1% % NBS Traceable Analysis Dates: First      Last 9/18/87

P-0724 CYLINDER PRESSURE 2000 PSIG

### CERTIFICATE OF ANALYSIS - EPA PROTOCOL GASES\*

(Concentrations are in mole % or ppm)

COMPONENTS	CERTIFIED CONC	EXPIRATION DATE	ANALYTICAL PRINCIPLE	PRIMARY STANDARD NBS/SRM'S	REPLICATE CONCENTRATIONS FIRST	REPLICATE CONCENTRATIONS SECOND
OXYGEN	13.13%	3/18/89	BECKMAN PARAMAGNETIC	2659 CAL-5911	13.12%	13.12%
NITROGEN	BALANCE			2651 CAL-4155	13.14%	
				5.07%		

Cylinder Number      Certified Accuracy      % NBS Traceable Analysis Dates: First      Last     

COMPONENTS	CERTIFIED CONC	EXPIRATION DATE	ANALYTICAL PRINCIPLE	PRIMARY STANDARD NBS/SRM'S	REPLICATE CONCENTRATIONS FIRST	REPLICATE CONCENTRATIONS SECOND

\*We hereby certify the cylinder gas has been analyzed according to EPA Protocol No:     

Analyst *Vito G...* Approved By *J Shapiro*

The only liability of this Company for gas which fails to comply with this analysis shall be replacement thereof by the Company without extra cost.

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OXYGEN CYLINDER CERTIFICATION

Company: Liquid Carbonic

Analyst: Troy LeSage

Cylinder # SGAL 2875

Date: 6/22/88

Instrument: Orsat Analysis

<u>Trial</u>	<u>O<sub>2</sub></u>	<u>CO<sub>2</sub></u>
1	19.7	0.0
2	19.8	0.0
3	29.9	0.0
4	19.9	0.0
5	19.9	0.0
6	20.0	0.0
7	20.0	0.0
8	19.8	0.0
9	19.9	0.0
10	19.9	0.0
11	20.0	0.0
12	<u>19.9</u>	<u>0.0</u>
	Total	238.7
		0.0

Mean O<sub>2</sub> = 19.89%