

The file name refers to the reference number, the AP42 chapter and section. The file name "ref02_c01s02.pdf" would mean the reference is from AP42 chapter 1 section 2. The reference may be from a previous version of the section and no longer cited. The primary source should always be checked.

Reference 146

EXPLOSIVES
AP-42 Section 5.6
Reference Number
2

From NAME Georgia

NO_2 Nitration Reactors

$$= \frac{0.0816}{16 \text{ TNT}} \times 2000 = 160 \frac{16 \text{ NO}_2}{\text{ton}}$$

Direct Process

~~CONCENTRATORS~~ AOP Plant

$$\frac{1.5416 \text{ NO}_2}{\text{ton HNO}_3} \times \frac{156 \text{ ton HNO}_3}{195 \text{ ton TNT}} \times 1 \frac{16}{\text{ton TNT}}$$

[SAR]

$$8.1 \frac{\# \text{ SO}_2}{\text{ton alum}} \times \frac{428 \text{ ton alum}}{195 \text{ ton TNT}} = 17.8 \text{ or } 18$$

NAUM
→ $0.4 \frac{16 \text{ mist}}{\text{ton TNT}}$

Red Water Incin.

$$0.35 \frac{\text{gr}}{\text{SCF}} \times \frac{4500 \text{ SCFM}}{5 \text{ GPM } 35\% \text{ solids}} \times \frac{0.62 \text{ GAL red}}{16 \text{ TNT}} \times \frac{200016}{\text{ton}} \frac{16}{\text{ton}}$$

$$\frac{(0.35)(0.62)(4500)(2000)}{7000 (5)} =$$

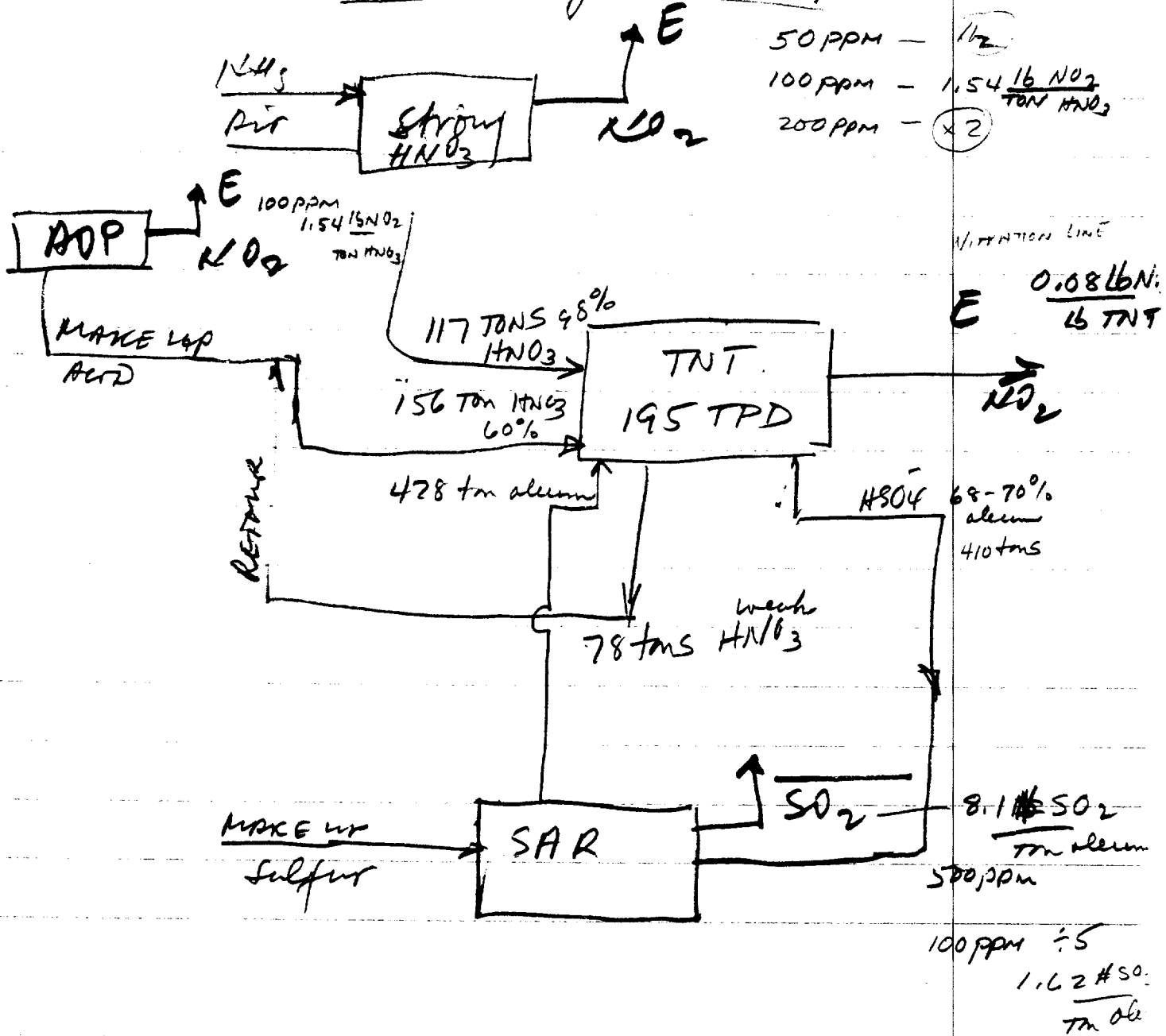
$$28 \approx 30$$

$$+ \text{Ref. } 70$$

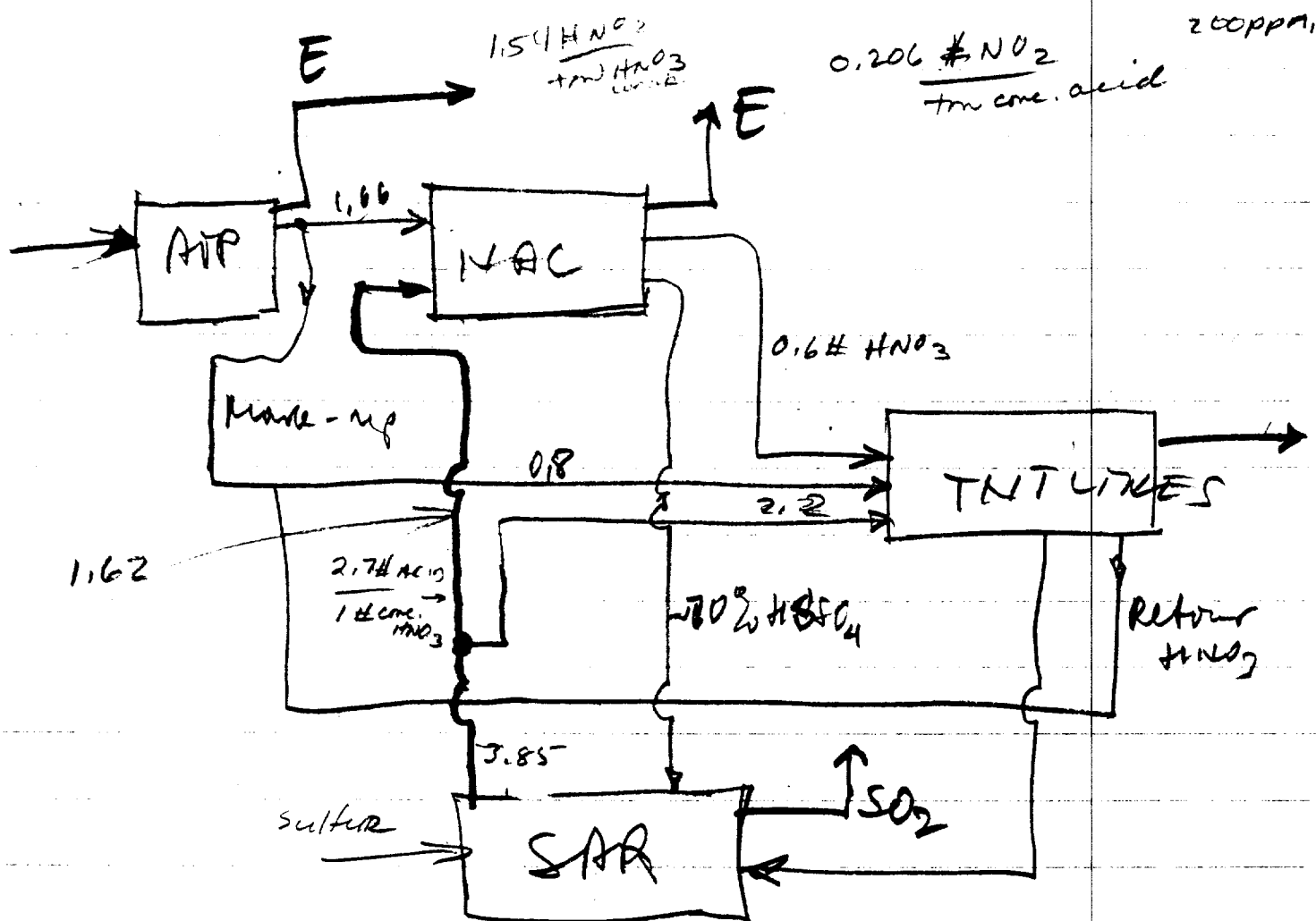
$$\frac{100}{2} = 50$$

$$36$$

Direct process



INDIRECT PROCESS



2.46 # AOP acid / # TNT

3.85 # H₂SO₄ / # TNT

2.2 # H₂SO₄ → 1 # HNO₃ conc. acid

SAR

100 ~~FF~~ RD

0.152 15

ton TNT

1 mg H_2SO_4
SCF gas

0.18 16 ^{air}

ton H_2SO_4

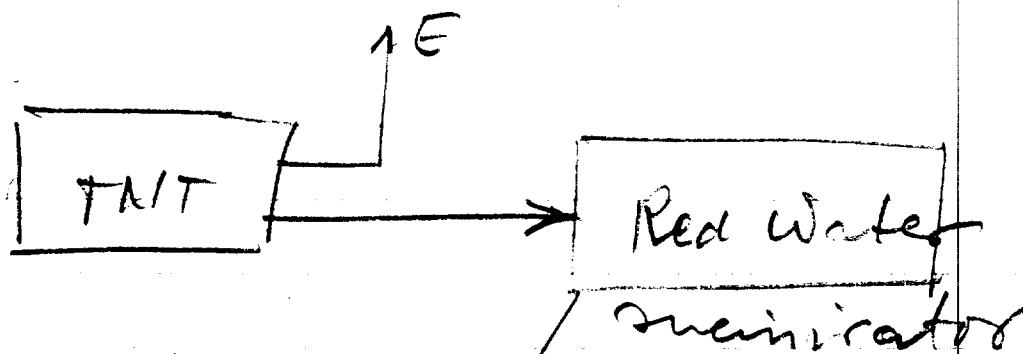
2.2 15 H_2

15 TNT

0.364 15 acid mist
ton TNT

0.62 gal red water

~~15~~ 16 TNT



1360 ppm NO_2

4500 scfm

5 gal/min

0.351 gr Part
dry scf

Red water

TNT

5.1 pounds red water

pound TNT

~~45~~ 15 Part
gal red water

35-40% solids
water

5 gal 1.65 mils

$$0.35 \frac{\text{gr}}{\text{scf}} \times \frac{900 \text{ scf}}{\text{gal}} \times \frac{1 \text{ lb}}{7000 \text{ gr}} = 0.045 \frac{\text{lb}}{\text{gal}}$$

$$\frac{0.52 \text{ lb Part}}{1 \text{ lb}} \times \frac{1 \text{ lb}}{1000}$$

HNO_3 AOP Process $1.54 \text{ lb } NO_2$
 $\text{tn } HNO_3$

concent new $0.2 \frac{\#}{\text{tn}}$ new $\approx 2 \text{ lb } NO_2$
 $\text{tn } HNO_3$

old $20 \frac{\#}{\text{tn}}$ old plant $\approx 57 \text{ lb } NO_2$
 $\text{tn } HNO_3$

TNT	Part	90x	NOx
NITRATION LINE	-	-	160
NITRIC ACID ^{mntg.} 6000	-	-	2-58
Sulfuric Acid Regenerator	-	5	-
RED WATER INCINERATOR $\frac{450}{5}$ 70		13	6

Nitrocellulose

Sulfuric Acid Core

ppm

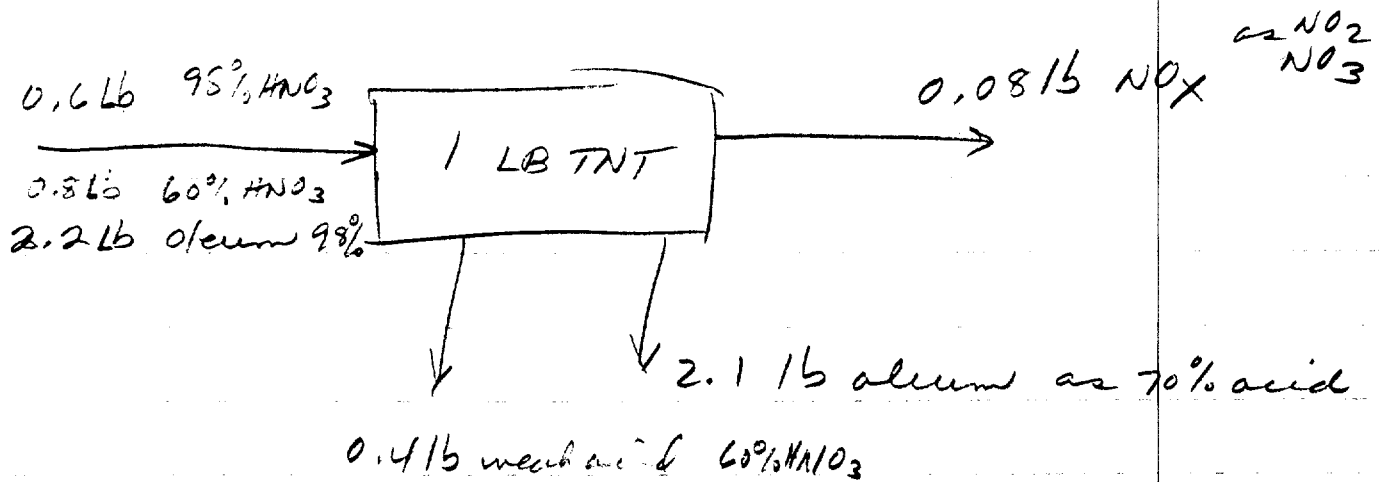
$0.35 \frac{\text{gr}}{\text{SCF}} \times \frac{900}{4500 \text{ SCF}} = \frac{1 \text{ lb}}{7000 \text{ gr}}$ $0.045 \text{ lb Part gal}$

$\frac{450}{5} = \text{Part}$
 $\frac{1 \text{ lb}}{\text{gal}}$

$\frac{900}{35} = 25.71$
 $\frac{4500}{31500}$

$\frac{10,000}{1045} = 9.56$
 $\frac{450000}{400000}$

$0.045 \text{ lb Part gal} \times \frac{1 \text{ gal}}{15} = 5.1 \text{ lb} \approx 2000 \text{ p. mt}$



AOP Ammonia Oxid. Process (60% acid)

Direct Process For Mntg, Strong HNO_3

50 ppm