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Research Triangle Park, North Carolina,**

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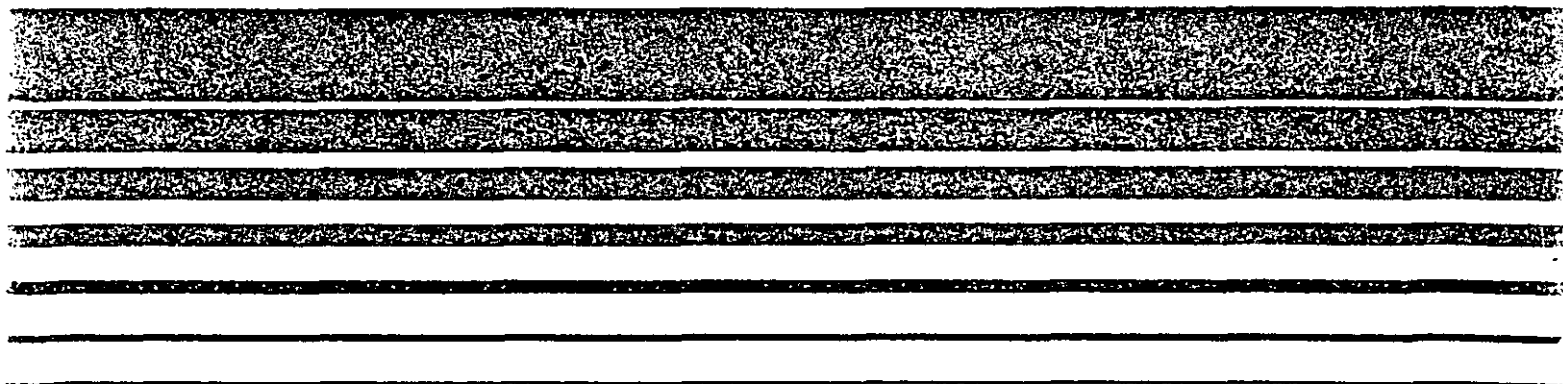
Air



Ammonium Sulfate

Facility D

Emission Test Report Chevron Chemical Richmond, California



SET #2632-01-0179

FINAL REPORT

PARTICULATE EMISSIONS FROM AN
AMMONIUM SULFATE PLANT
CONTROLLED BY A VENTURI SCRUBBER

EPA Contract No. 68-02-2813
Work Assignment No. 26

Prepared for:

Environmental Protection Agency
Emission Measurement Branch
ESED Mail Drop #13
Research Triangle Park, N.C. 27711

May 29, 1979

SCOTT ENVIRONMENTAL TECHNOLOGY, INC.
2600 Cajon Boulevard
San Bernardino, California 92411



Scott Environmental Technology Inc.

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1.0 INTRODUCTION

Testing to determine particulate emissions from an ammonium sulfate plant was conducted by Scott Environmental Technology, Inc. for the U.S. Environmental Protection Agency under Contract No. 68-02-2813, Work Assignment No. 26. Three tests were conducted on December 12 and 13, 1978 at the Chevron Chemical Company ammonium sulfate plant located in Richmond, California.

Particulate tests were conducted at the inlet and outlet of a venturi scrubber controlling emissions in the exhaust gases from an ammonium sulfate drier using EPA Method #5. One test to determine particle size distribution was also performed at the inlet to the scrubber using an Andersen 2000 Cascade Impactor. Opacity of the gas exiting from the scrubber was recorded during each test by a smoke reader. Samples of the ammonium sulfate crystals were collected at the inlet and outlet of the drier to determine moisture content. Also, samples of the scrubber liquor were collected downstream from the scrubber.

The test arrangements were made through William Moriarty, Manager of Operations, Manufacturing, with Chevron Chemical Company. Dennis Holzschuh of the EPA was present during the tests as was Marvin Drabkin of Mitre Corporation who monitored the plant process.



2.0 SUMMARY OF RESULTS

The particulate concentration at the outlet of the scrubber ranged from 0.0516 to 0.122 grains/scf and averaged 0.084 grains/scf for the three runs. The average gas flow rate was 4038 dscfm resulting in an average particulate mass flow rate of 3.0 lbs/hour. Inlet particulate concentrations averaged 43.8 grains/scf with an average gas flow rate of 3803 dscfm and particulate mass flow rate of 1424 lbs/hour. The collection efficiency of the scrubber was 99.9% for Test Run No. 2. Complete Method #5 results are summarized in Table 2.1.

The results of the particulate size distribution sample are shown in tabular and graphical form in Table 2.2 and Figure 2.1, respectively.

The average moisture content of the ammonium sulfate crystals was 0.54% at the drier inlet and 0.19% at the drier outlet. Complete results are shown in Table 2.3.

The opacity at the outlet averaged 0% during each test. Results of the opacity readings are summarized in Tables 2.4 through 2.7.

The field data sheets are included in Appendix A.



FINAL REPORT

TABLE 2.1
SUMMARY OF METHOD #5
RESULTS

TABLE 2.1 SUMMARY OF METHOD #5 RESULTS	Location	Inlet			Outlet		
	Run No.	2	3	4	1	2	3
Chevron Chemical Company Date: 12/12 & 12/13/78	Date	12/12	12/13	12/13	12/12	12/12	12/13
	Time Started	1540	0850	1330	1245	1705	0902
	Time Ended	1730	1100	1420	1504	1921	1124
Barometric Pressure: P_{bar} (in. Hg.)		30.31	30.35	30.35	30.26	30.25	30.35
Static Pressure: P_q (in. H_2O)		-0.05	-0.05	-0.05	1.0	1.0	1.0
Area of Stack: A (ft ²)		2.50	2.50	2.50	1.23	1.23	1.23
Pitot Coefficient: C_p		0.838	0.838	0.838	0.835	0.835	0.835
Meter Calibration Factor: Y		0.94	0.94	0.94	1.075	1.075	1.075
Area of Nozzle: A_n (in ²)		0.0491	0.0491	0.0491	0.035	0.035	0.035
Total Sampling Time: Θ (Min.)		90	90	24.75	128	128	128
Gas Sample Volume: V_m (ft ³)		47.225	42.429	12.390	91.509	87.924	98.371
Avg. Velocity Head: $(\sqrt{\Delta p})^2_{avg}$ (in. H_2O)		0.25	0.20	0.251 0.302	1.16	1.04	1.30
Avg. Orifice Pressure: ΔH (in H_2O)		0.84	0.70	0.83	1.97	1.76	2.19
Avg. Stack Temperature: T_s (°R)		638	636	641	574	571	574
Avg. Meter Temperature: T_m (°R)		550	536	540	537	547	546
Volume of Liquid and Silica Gel Collected: V_{lc} (ml.)		73	56	16	166	151	185
Gas Sample Volume @ Std. Cond.: $V_m(Std) \text{ (ft}^3\text{)} = \frac{17.64 V_m Y}{T_m} (P_{bar} + \Delta H/13.6)$		43.242	39.904	11.570	98.252	92.599	104.241
Volume of Water Vapor: $V_w(Std) \text{ (ft}^3\text{)} = 0.04707 V_{lc}$		3.44	2.64	0.753	7.81	7.11	8.71
Moisture Content: $B_{ws} = \frac{V_w(Std)}{V_m(Std) + V_w(Std)}$		0.074	0.062	0.061	0.074	0.071	0.077
Molecular Weight of Stack Gas (dry): $M_d = 0.44 (\% CO_2) + 0.32 (\% O_2) +$ $0.28 (\% N_2 + \% CO)$		28.90	28.90	28.90	28.82	28.86	28.86

¹ Average during sampling.² Average in entire duct.

Location	Inlet			Outlet		
Run Number	2	3	4	1	2	3
Molecular Weight of Stack Gas (wet): $M_s = M_d (1-B_{ws}) + 18.0 B_{ws}$	28.09	28.22	28.24	28.02	28.09	28.02
Stack Pressure: P_s (in. Hg) = $P_{bar} + P_g/13.6$	30.31	30.35	30.35	30.33	30.32	30.42
Stack Gas Velocity: v_s (ft/sec) = $85.49 C_p (\Delta P_s / P_s M_s)^{1/2}$	31.01	27.61	30.98 ¹ 33.93 ²	63.19	59.61	66.79
Stack Gas Volume Flow Rate: Q_{sd} (dscfh/min) = $1059 (1-B_{ws}) v_s A P_s / T_s$	3612	3272 ³	3994 ²	4027	3830	4256
Actual Stack Gas Volume Flow Rate: Q (acfh/min) = $60 v_s A$	4652	4142	5090 ²	4663	4399	4929
Weight of Particulate Collected: m_n (mg.)	127541.4	64757.4	31554.2	502.9	310.1	825.1
Concentration of Particulate @ Std.Cond.(dry): C_s (gr/scf) = $0.01542 m_n / V_m$ (std) $[C_s$ (g/dscm) = $0.03529 m_n / V_m$ (std)]	45.48 [104.1]	25.02 ³ 57.27	42.05 96.24	0.0789 0.181	0.0516 0.118	0.122 0.279
Mass Flow Rate of Particulate: Q (lb/hr) = $0.008571 C_s Q_{sd}$	1408	701.7 ³	1439	2.7	1.7	4.5
Isokinetic Rate: I (%) = $13.61 T_s V_m$ (std) / $P_s v_s A_n \ominus (1-B_{ws})$	97.6	99.4	94.1	96.5	95.7	96.9
Control Efficiency, %				----	99.9	99.4 ³

¹ Average during sampling.

² Average in entire duct.

³ Not included in average due to leak in sample train.



TABLE 2.2
PARTICLE SIZE DISTRIBUTION

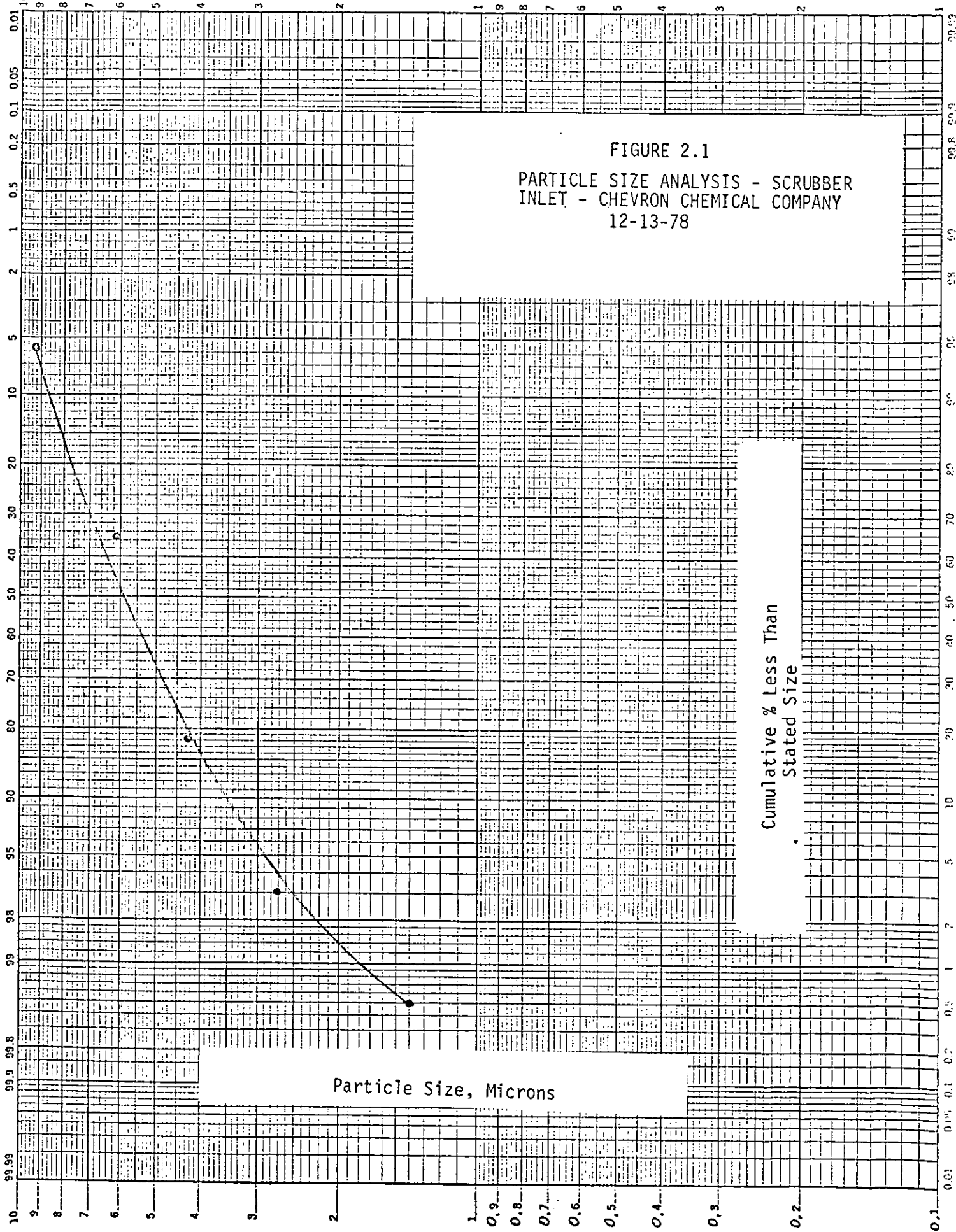
Date:	December 13, 1978	P _{bar} (in. Hg.)	30.35
Location:	Chevron	Stack Temp (°F)	178
Sampling Location:	Inlet	Sample Time (Min)	2
Traverse Point No. Sampled: 19		Sample Volume (cf)	0.937
		Moisture (% H ₂ O)	6.1
		Meter Temp (°F)	76
		Flow Setting, ΔH (in. H ₂ O)	0.67
		Nozzle Diameter (in.)	0.250

Sample Flow Rate (at stack conditions): 0.50 cfm

<u>Plate No.</u>	<u>Net Wt. (mg)</u>	<u>%</u>	<u>Cumulative %</u>	<u>ECD (Microns)</u>
1	157.3	5.8	100.0	14.73 and larger
2	789.5	29.1	94.2	9.28
3	1271.6	46.8	65.1	6.15
4	413.8	15.2	18.3	4.26
5	71.2	2.6	3.1	2.71
6	13.2	0.5	0.5	1.40
7	0.5	0.0	0.0	0.85
8	0.0	0.0	0.0	0.58
Backup Filter	0.3	0.0	0.0	<0.58
TOTAL	2717.4			



FIGURE 2.1
PARTICLE SIZE ANALYSIS - SCRUBBER
INLET - CHEVRON CHEMICAL COMPANY
12-13-78



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TABLE 2.3

AMMONIUM SULFATE CRYSTAL
MOISTURE ANALYSIS

<u>Date</u>	<u>Time</u>	<u>Test Run No.</u>	<u>Sample Location</u>	<u>Net Wt. Wet, Gms.</u>	<u>Net Wt. Dry, Gms.</u>	<u>Moisture %</u>
12-12-78	1442	1	Inlet	361.0	358.8	0.61
12-12-78	1440	1	Outlet	344.3	343.7	0.17
12-12-78	1712	2	Inlet	372.1	370.2	0.51
12-12-78	1716	2	Outlet	386.6	385.6	0.26
12-13-78	1119	3	Inlet	409.1	407.0	0.51
12-13-78	1117	3	Outlet	392.3	391.8	0.13

Average at drier inlet - 0.54

Average at drier outlet - 0.19



TABLE 2.4
SUMMARY OF RESULTS OF OPACITY READINGS

Location: Scrubber Outlet

Stack Height: 20 feet

Test Run No.: 1

Distance to Stack: 150 feet

Date: 12-12-78

Wind Direction: South Speed: 0-20 MPH

Color of Plume: White

Sky Description: Gray Clouds - 75%

Note: Readings every 30 seconds; therefore, average opacity = sum/12

Set Number	Time		Opacity		Set Number	Time		Opacity	
	Start	End	Sum	Average		Start	End	Sum	Average
1	1230	1236	5	0					
2	1236	1242	35	5					
3	1247	1253	15	0					
4	1253	1259	15	0					
5	1259	1305	30	0					
6	1304	1311	15	0					
7	1311	1317	10	0					
8	1317	1323	20	0					
9	1323	1329	25	0					
10	1329	1335	10	0					
11	1335	1341	20	0					
12	1341	1347	15	0					
13	1347	1353	35	5					
14	1353	1359	35	5					
15	1359	1405	0	0					
16	1405	1411	15	0					
17	1411	1417	15	0					
18	1417	1423	10	0					
19	1423	1429	5	0					

OVERALL AVERAGE: 0



TABLE 2.5
SUMMARY OF RESULTS OF OPACITY READINGS

Location: Scrubber Outlet

Test Run No.: 2

Date: 12-12-78

Color of Plume: White

Stack Height: 20 feet

Distance to Stack: 150 feet

Wind Direction: South Speed: 10-20 MPH

Sky Description: Gray clouds - 75%

Note: Readings taken every 30 seconds; therefore, average opacity = sum/12.

Set Number	Time		Opacity	
	Start	End	Sum	Average
1	1540	1546	15	0
2	1546	1552	10	0
3	1552	1558	5	0
4	1558	1604	15	0
5	1604	1610	10	0
6	1610	1616	10	0
7	1616	1622	20	0
8	1622	1628	15	0
9	1628	1634	10	0
10	1634	1640	10	0
11	1640	1646	5	0
12	1646	1652	5	0
13	1652	1658	20	0
14	1658	1704	5	0
15	1704	1710	5	0

Set Number	Time		Opacity	
	Start	End	Sum	Average

OVERALL AVERAGE: 0



TABLE 2.6
SUMMARY OF RESULTS OF OPACITY READINGS

Location: Scrubber Outlet

Test Run No.: 3

Date: 12-13-78

Color of Plume: White

Stack Height: 20 feet

Distance to Stack: 150 feet

Wind Direction: South Speed: 0-10 MPH

Sky Description: White Clouds - 50%

Note: Readings taken every 30 seconds; therefore, average opacity = sum/12.

Set Number	Time		Opacity		Set Number	Time		Opacity	
	Start	End	Sum	Average		Start	End	Sum	Average
1	0848	0854	5	0	21	1048	1054	0	0
2	0854	0900	0	0	22	1054	1100	5	0
3	0900	0906	5	0	23	1100	1106	0	0
4	0906	0912	5	0	24	1106	1112	0	0
5	0912	0918	0	0	25	1155	1201	0	0
6	0918	0924	0	0	26	1201	1207	5	0
7	0924	0930	5	0	27	1207	1213	5	0
8	0930	0936	0	0	28	1213	1219	0	0
9	0936	0942	5	0	29	1219	1225	5	0
10	0942	0948	0	0					
11	0948	0954	0	0					
12	0954	1000	5	0					
13	1000	1006	0	0					
14	1006	1012	10	0					
15	1012	1018	5	0					
16	1018	1024	0	0					
17	1024	1030	15	0					
18	1030	1036	0	0					
19	1036	1042	5	0					
20	1042	1048	0	0					

OVERALL AVERAGE: 0



TABLE 2.7
SUMMARY OF RESULTS OF OPACITY READINGS

Location: Scrubber Outlet

Stack Height: 20 feet

Test Run No.: 4

Distance to Stack: 150 feet

Date: 12-13-78

Wind Direction: South Speed: 0-15 MPH

Color of Plume: White

Sky Description: Clear

Note: Readings taken every 30 seconds; therefore, average opacity = sum/12.

Set Number	Time		Opacity	
	Start	End	Sum	Average
1	1437	1443	20	0
2	1443	1449	20	0
3	1449	1455	10	0
4	1455	1501	15	0

Set Number	Time		Opacity	
	Start	End	Sum	Average

OVERALL AVERAGE: 0



3.0 DISCUSSION OF RESULTS

A 40 inch stack extension was installed on the outlet of the dropout chamber in order to provide the necessary length of straight duct. Due to the cyclonic flow leaving the dropout chamber, it was also necessary to install a flow straightener in the duct.

Run No. 1 at the scrubber inlet was aborted due to a ruptured sample filter. The rupture was apparently caused by pressure surges in the sample train due to clogging of the nozzle and probe by the particulate. Clogging of the nozzle and probe was a problem during each test. During Runs No. 2 and 3, sampling was interrupted several times to clean the nozzle and probe. At the completion of sampling during Run No. 3, a leak was detected in the inlet sample train in a fitting in an umbilical line. Therefore, an additional test run (Number 4) was made at the inlet. Sampling was halted during Run No. 4 after the sampling traverse was completed for the center sample port due to the large amount of particulate collected. A velocity traverse only was performed on the remaining sample points.

Particle size sampling was conducted for only two minutes. However, due to the high concentration of large particles in the gas stream, the first few collecting plates were overloaded with particulate. Using a cyclone pre-separator, perhaps in an out-of-stack configuration, may have improved the sampling. Immediately after the sampling was completed, the collection plates were sealed in individual containers to avoid the loss of any sample. Particulate collected in the sample nozzle and sample head was included as part of Plate No. 1.



4.0 PROCESS DESCRIPTION AND OPERATION

The Chevron Chemical plant is designed to produce 220 TPD of ammonium sulfate (AS) from ammonia and sulfuric acid. All of the AS produced is sold for use as fertilizer. The plant operates continuously 24 hours a day for periods up to 5 to 6 weeks between short periods of maintenance. Varying AS market conditions during the year also affect the length of plant shut-down periods.

A. Process Description

Figure 4.1 shows a simplified diagram of the AS process and the sampling locations. Sulfuric acid (98 percent) and anhydrous ammonia are combined in a reactor or "saturator." The heat of reaction provides the energy for evaporation. As the concentration increases, the AS solution becomes saturated. AS crystals then form and are allowed to grow in size. The crystal slurry is fed to a centrifuge, which separates most of the liquid from the crystals. The wet crystals are then passed through a gas-fired rotary drum dryer, screened, and conveyed to a storage warehouse. A venturi scrubber with a liquid-to-gas ratio of 26 gal/1000 acf and a pressure drop of 13 inches of water is used to control dryer emissions.

B. Process Operation

The purpose of the test program was to measure emission levels from the venturi scrubber controlling dryer emissions. Process conditions were carefully observed, and testing was performed only during periods when the plant production rate was normal. During the tests, pertinent operating

conditions were monitored and recorded on process data sheets. These sheets are included in Appendix B.

As shown by Table 1 of Appendix B, the plant operated at a production rate very near the design capacity of 220 TPD during the emission tests. No calibrated weigh belts were used. The ammonium sulfate production rate was calculated from both the sulfuric acid and ammonia flow rates. According to plant personnel, the sulfuric acid flow rate is a more accurate basis for computing the production rate than the ammonia flow rate. The accuracy of the AS production rate based on acid flow is estimated to be within ± 5 percent.

The following parameters were monitored during the tests to verify that the dryer was operating normally:

1. Sulfuric acid flow rate
2. Ammonia flow rate
3. AS product weigh belt reading (uncalibrated)
4. Dryer operating temperatures
5. Centrifuge amperage
6. Crystallizer liquor level, temperature, vacuum
7. Percent free acid in crystallizer elutriation leg
8. AS slurry surge tank level
9. AS specific gravity of slurry

Process monitoring began approximately 1 hour before the start of emission Test Number 1 on the morning of December 12, 1978. Actual emission testing began at 12:45 p.m. for the scrubber inlet and 1:40 p.m.

for the scrubber outlet. The scrubber inlet test terminated at 3:00 p.m. (120 minutes net); the outlet test ended at 4:10 p.m. (120 minutes net). The process operation appeared to operate at steady state without interruption during this period.

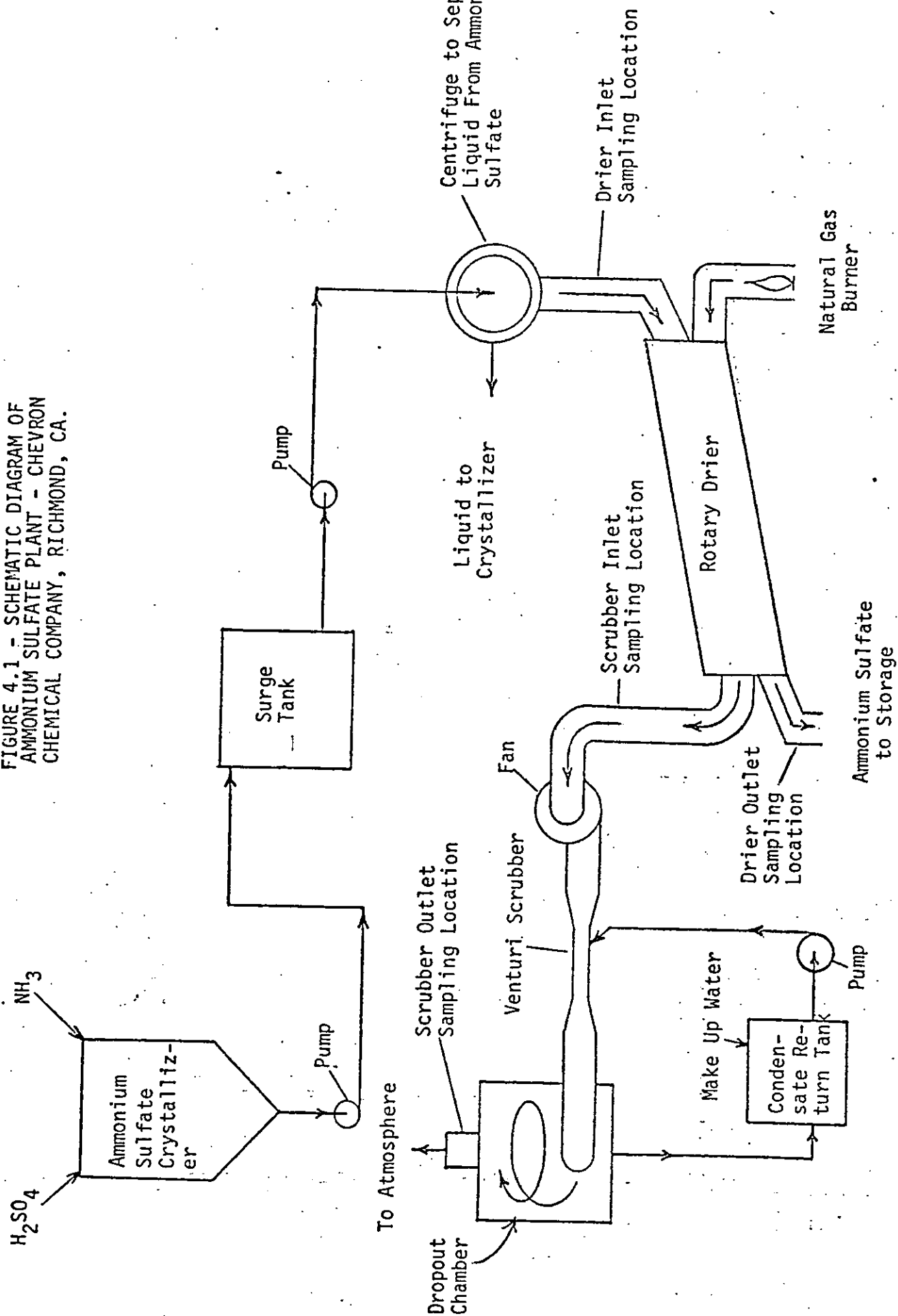
Monitoring for Test Number 2 began at 3:30 p.m. (scrubber inlet) and 4:54 p.m. (scrubber outlet). In this run, the scrubber inlet test terminated at 5:15 p.m., and the outlet test ended at 7:18 p.m.

Approximately half-way through the second test, it became apparent from the weigh belt readings that the AS production rate had dropped off significantly (even though sulfuric acid and ammonia flows remained constant). According to plant personnel, the flow of oxalic acid (a crystal growth promoter) to the crystallizer had been stopped, and the percentage of fines in the AS slurry leaving this unit had increased. In order to decrease the fines percentage in the product, the hold-up time in the crystallizer was increased by reducing the AS slurry flow to the centrifuge. This resulted in about a 10 to 15 percent drop in the rate of AS passing through the dryer during a brief portion of the test period. This drop in AS dryer throughput is not believed to have significantly affected the test results.

Test Number 3 began at 9:00 a.m. (scrubber outlet) and ended at 11:15 a.m. (scrubber outlet) on December 13, 1978. The scrubber inlet portion of the test was aborted due to problems of continual AS blockage in the equipment. It was decided that the 2 scrubber inlet tests completed on December 12 were adequate. A particle size distribution test

was done at the scrubber inlet, however. The AS production rate was normal during the test period although the AS crystal size distribution had not completely returned to normal.

FIGURE 4.1 - SCHEMATIC DIAGRAM OF AMMONIUM SULFATE PLANT - CHEVRON CHEMICAL COMPANY, RICHMOND, CA.



5.0 SAMPLING AND ANALYTICAL PROCEDURES

Gas sampling for total particulate content was conducted at the inlet and outlet of the scrubber in accordance with EPA Reference Method #5. This method involves the isokinetic extraction of a sample from the gas stream and collection of the particulate on a heated out-of-stack filter. A dry gas meter measures the volume of the gas sample. The gas velocity in the duct is measured during the sampling with a Pitot tube and inclined manometer. The stack gas temperature is measured with a chromel-alumel thermocouple. The quantity of particulate collected is determined gravimetrically with results reported as grains of particulate per standard cubic foot of gas and grams per cubic meter.

The sample for particle size distribution was collected using an Andersen 2000 In-Stack Cascade Impactor. The particles are collected by impaction on a series of plates. The plates have increasingly smaller holes so that the velocity of the particles is increased from plate to plate and smaller and smaller particles are impacted. The particulate weight collected on each plate is determined gravimetrically. The particle size distribution is based on the equivalent aerodynamic size of the particles based on spherical particles of 1 gram/cc density.

Opacity readings of the scrubber outlet gases were made in accordance with EPA Method #9. The moisture content of the ammonium sulfate samples from the drier inlet and outlet was determined by weighing the samples before and after drying.



APPENDIX A
FIELD DATA SHEETS



PLANT CHEVRON ORTHO - RICHMOND
DATE 12-12-78
SAMPLING LOCATION OUTLET
SAMPLE TYPE METHOD 5
RUN NUMBER OUTLET #1
OPERATORS JP, JP
AMBIENT TEMPERATURE
BAROMETER 30.26

PROBE LENGTH & TYPE 2' GLASS
NOZZLE I.D. 0.10
SAMPLE BOX NUMBER 60001
METER BOX NUMBER SAO "B" 2 = 1005
PROBE HEATER SETTING VOLTAIC 11
FILTER HEATER SETTING 30
REFERENCE ΔP 1.90
READ AND RECORD ALL DATA EVERY 4 MINUTES

FYRITE ANALYSIS
CO₂ O₂

SAMPLE CORRECTION

12-30 103
12-30 173
12-30 173

START TIME 1245

TRAVERSE POINT NUMBER	CLOCK TIME (24-hr CLOCK)	GAS METER READING (V _m , ft ³)	VELOCITY HEAD (49.2), in. H ₂ O	ORIFICE PRESSURE DIFFERENTIAL (49.2), in. H ₂ O		STACK TEMPERATURE (T _s), °F	DRY GAS METER TEMPERATURE (T _m), °F		PUMP VACUUM, in. Hg	IMPIGNER TEMPERATURE, °F	THERMOCouple TEMP. °F	COMMENTS
				DESIRED	ACTUAL		INLET (T _{m in}), °F	OUTLET (T _{m out}), °F				
1	4	270.100	1.2	2.0	2.0	113	62	62	3.3			Box 297 PROBE 111
2	8	272.850	1.05	1.8	1.8	112	68	69	3.2			Box 284 PROBE 107
3	12	275.508	1.05	1.9	1.9	113	74	69	3.0			Box 268 PROBE 155
4	16	278.210	1.1	1.9	1.9	113	76	68	2.9			Box 285 PROBE 111
5	20	280.905	1.05	1.8	1.8	113	78	68	3.2			Box 286 PROBE 107
6	24	283.710	1.2	2.0	2.0	113	81	68	3.5			Box 286 PROBE 111
7	28	286.728	1.3	2.3	2.3	113	82	67	4.2			Box 285 PROBE 108
8	32	289.912	1.5	2.5	2.5	114	84	66	3.5			Box 285 PROBE 108
9	36	292.740	1.1	1.85	1.85	114	85	68	3.7			Box 285 PROBE 108
10	40	295.610	1.2	2.0	2.0	114	86	68	3.7			Box 285 PROBE 108
11	44	298.500	1.2	2.0	2.0	115	88	69	3.8			Box 285 PROBE 108
12	48	301.310	1.1	1.85	1.85	114	89	70	3.7			Box 285 PROBE 108
13	52	304.130	1.1	1.85	1.85	115	89	70	3.6			Box 285 PROBE 108
14	56	306.940	1.1	1.85	1.85	114	90	70	3.5			Box 285 PROBE 108
15	60	309.710	1.1	1.85	1.85	114	90	70	3.5			Box 285 PROBE 108
16	64	312.513	1.05	1.8	1.8	115	91	71	3.5			Box 285 PROBE 108
17	8 1400	314.995	1.1	1.85	1.85	116	79	69	3.5			Box 277 PROBE 160
18	12	317.965	1.1	1.65	1.65	117	80	70	3.5			Box 282 PROBE 152
19	16	320.100	1.0	1.6	1.6	117	80	70	3.4			Box 282 PROBE 150

[illegible]

TRAVERSE POINT LOCATION & VELOCITY DATA BY

TRAVERSE POINT NUMBER	A=FRACTION OF I.D.	B=AxI.D. ID=	C=B+NIPPLE NIPPLE=	VELOCITY HEAD (Δp_s), in.H ₂ O	STACK TEMPERATURE (T_s), °F
1				1.02	111
2				1.02	112
3				1.02	112
4				1.02	112
5				1.02	112
6				1.02	112
7				1.02	112
8				1.02	112
9				1.02	112
10				1.02	112
11				1.02	112
12				1.02	112
13				1.02	112
14				1.02	112
15				1.02	112
16				1.02	112
17				1.1	114
18				1.05	113
19				1.05	113
20				.98	113
21				.98	113
22				1.1	113
23				1.3	113
24				1.5	113
25				1.5	113
26				1.5	113
27				1.3	113
28				1.2	113
29				1.1	114
30				1.1	114
31				1.2	114
32				1.2	114
33					
34					
35					
36					
37					
38					
39					
40					
41					
42					
43					
44					
45					
46					
47					
48					
AVERAGE					

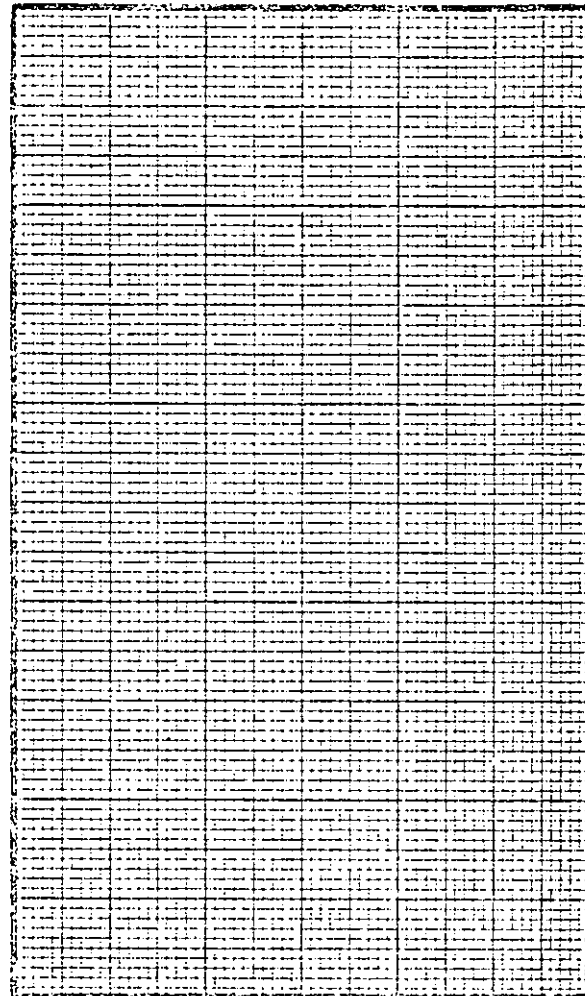


DIAGRAM OF STACK, PORTS, & TRAVERSE
POINTS (indicate direction of flow)

INSIDE DIMENSIONS OF SAMPLE PLANE

15" CIRCULAR

STACK GAUGE PRESSURE in. H₂O ⁽⁺⁾1.0

NEAREST UPSTREAM DISTURBANCE

NEAREST DOWNSTREAM DISTURBANCE

PROCESS & CONTROL EQUIPMENT
DESCRIPTION



SCOTT ENVIRONMENTAL TECHNOLOGY, INC.

MOISTURE

IMPINGERS

FINAL VOLUME 332 ml
INITIAL VOLUME 200 ml
NET VOLUME 132 ml

SILICA GEL

FINAL WEIGHT 501.9 g
INITIAL WEIGHT 468.0 g
NET WEIGHT 33.9 g
TOTAL MOISTURE 166 g

1 - 167
243 165

ANALYTICAL DATA BY _____

ACETONE FRONT WASH

FINAL 84.5148 mg
TARE 84.0444 mg
NET 470.4 mg

FILTER NUMBER 1

FINAL 4589 mg
TARE 042104 mg
NET 32.5 mg

FILTER NUMBER 2

FINAL 507.9 mg
TARE 46108 mg
NET 44.9 mg

FILTER NUMBER 3

FINAL mg
TARE mg
NET mg

CYCLOCNE

FINAL mg
TARE mg
NET mg

TOTAL FRONT

 mg

ACETONE BACK WASH

FINAL mg
TARE mg
NET mg

ETHER-CHLOROFORM EXTRACT

FINAL mg
TARE mg
NET mg

WATER EVAPORATION

FINAL mg
TARE mg
NET mg

TOTAL BACK

 mg

I CERTIFY THAT THE SAMPLES DESCRIBED BY THIS DATA SHEET WERE COLLECTED IN ACCORDANCE WITH METHODS OUTLINED BY _____

I FURTHER CERTIFY THAT THE SAMPLES WERE IN THE POSSESSION OF, OR SEALED FOR SHIPMENT BY COMMON CARRIER BY, MYSELF UNTIL DELIVERY TO A LABORATORY FOR ANALYSIS.

SIGNED _____ DATE _____
WITNESS _____ DATE _____
I CERTIFY THAT I RECEIVED THE SAMPLES DESCRIBED BY THIS DATA SHEET FROM THE ABOVE NAMED INDIVIDUAL AND ANALYZED THEM IN ACCORDANCE WITH THE ABOVE METHODS.

NOMOGRAPH DATA BY JBP

CALIBRATED PRESSURE DIFFERENTIAL ACROSS ORIFICE, in. H ₂ O	ΔH ₀	1.865
AVERAGE METER TEMPERATURE (AMBIENT + 20°F), °F	T _m avg.	80
PERCENT MOISTURE IN GAS STREAM BY VOLUME	B _{W0}	10
BAROMETRIC PRESSURE AT METER, in. Hg	P _m	30.26
STATIC PRESSURE IN STACK, in. Hg	P _s	7.69
P _m - 0.023 x STACK GAUGE PRESSURE (in. H ₂ O)	P _s /P _m	1.02
RATIO OF STATIC PRESSURE TO METER PRESSURE	T _s avg.	116
AVERAGE STACK TEMPERATURE, °F	ΔP avg.	3.5
AVERAGE VELOCITY HEAD, in. H ₂ O	ΔP max.	90
MAXIMUM VELOCITY HEAD, in. H ₂ O		20
C FACTOR		196
CALCULATED NOZZLE DIAMETER, in.		1.10
ACTUAL NOZZLE DIAMETER, in.		
REFERENCE ΔP, in. H ₂ O		

DRY MOLECULAR WEIGHT DETERMINATION BY _____

SAMPLING TIME (24-hr CLOCK) _____

SAMPLING LOCATION _____

SAMPLE TYPE (BAG, INTEGRATED, CONTINUOUS) _____

ANALYTICAL METHOD _____

AMBIENT TEMPERATURE _____

RUN	1		2		3	
	ACTUAL READING	NET	ACTUAL READING	NET	ACTUAL READING	NET
GAS						
CO ₂	100.0	0.0				
O ₂ (NET IS ACTUAL O ₂ READING MINUS ACTUAL CO ₂ READING)	79.6	20.4				
CO (NET IS ACTUAL CO READING MINUS ACTUAL O ₂ READING)		79.6				

FYRITE ANALYSIS

CO₂ O₂

PLANT CHEVRON CHEMICAL, RICHMOND PROBE LENGTH & TYPE 4" GALASS

NOZZLE I.D. .250

SAMPLE BOX NUMBER SCOTT SPURT BOX

METER BOX NUMBER SCOTT 303 1.875

PROBE HEATER SETTING 2500

FILTER HEATER SETTING 2500

REFERENCE ΔP .58

READ AND RECORD ALL DATA EVERY 15 MINUTES

DATE 12/12/78

SAMPLING LOCATION INLET

SAMPLE TYPE METHOD 5

RUN NUMBER 2

OPERATORS T.S. & W.D.

AMBIENT TEMPERATURE 60 @ 1535

BAROMETER 20.31 @ 1530

TRAVERSE POINT NUMBER	CLOCK TIME SAMPLING TIME, min	GAS METER READING (V _m), ft ³	VELOCITY HEAD (v _h), in. H ₂ O	ORIFICE PRESSURE DIFFERENTIAL (ΔH), in. H ₂ O		STACK TEMPERATURE (T _s), °F	DRY GAS METER TEMPERATURE		PUMP VACUUM, in. Hg	IMPINGER TEMPERATURE, °F	COMMENTS
				DESIRED	ACTUAL		INLET (T _{m in}), °F	OUTLET (T _{m out}), °F			
	0	INITIAL: 717.275									
1	7.5	718.982	.42	1.25	1.25	176	68	68	5.0		
2	10.0	720.440	.38	1.2	1.2	182	68	69	4.6		
3	12.5	722.278	.37	1.2	1.2	181	73	70	4.2		
4	15.0	723.885	.37	1.2	1.2	177	75	71	4.5		1500°F 770°F
5	17.5	725.502	.35	1.13	1.13	176	79	72	4.5	60	
6	20.0	726.930	.27	.86	.86	173	85	74	3.5		
7	22.5	728.276	.27	.86	.86	171	85	76	3.5		
8	25.0	729.561	.24	.77	.77	171	88	77	3.5		
9	27.5	730.930	.27	.96	.96	169	89	78	3.5		
10	30.0	732.320	.31	1.0	1.0	174	91	80	4.0		
11	32.5	734.031	.42	1.35	1.35	176	93	81	5.2		
12	35.0	735.779	.42	1.35	1.35	177	95	82	5.2		
13	37.5	736.691	.14	.46	.46	170	95	83	2.8		
14	40.0	737.530	.07	.235	.235	177	95	82	1.9		
15	42.5	738.237	.07	.235	.235	177	95	84	1.2		
16	45.0	739.030	.10	.23	.23	176	96	86	2.0		
17	47.5		.12	.235	.235	161	96	86	2.5		
18	50.0	741.039	.18	.50	.50	161	98	87	3.0		
19	52.5	742.1	.15	.30	.30	169	98	87	3.5		

TRAVERSE POINT LOCATION & VELOCITY DATA BY

TRAVERSE POINT NUMBER	A=FRACTION OF I.D.	B=AXI.D. ID=	C=B+NIPPLE NIPPLE=	VELOCITY HEAD (Δp_g), in. H ₂ O	STACK TEMPERATURE (T_g), °F
1					
2					
3					
4					
5					
6					
7					
8					
9					
10					
11					
12					
13					
14					
15					
16					
17					
18					
19					
20					
21					
22					
23					
24					
25					
26					
27					
28					
29					
30					
31					
32					
33					
34					
35					
36					
37					
38					
39					
40					
41					
42					
43					
44					
45					
46					
47					
48					
AVERAGE					

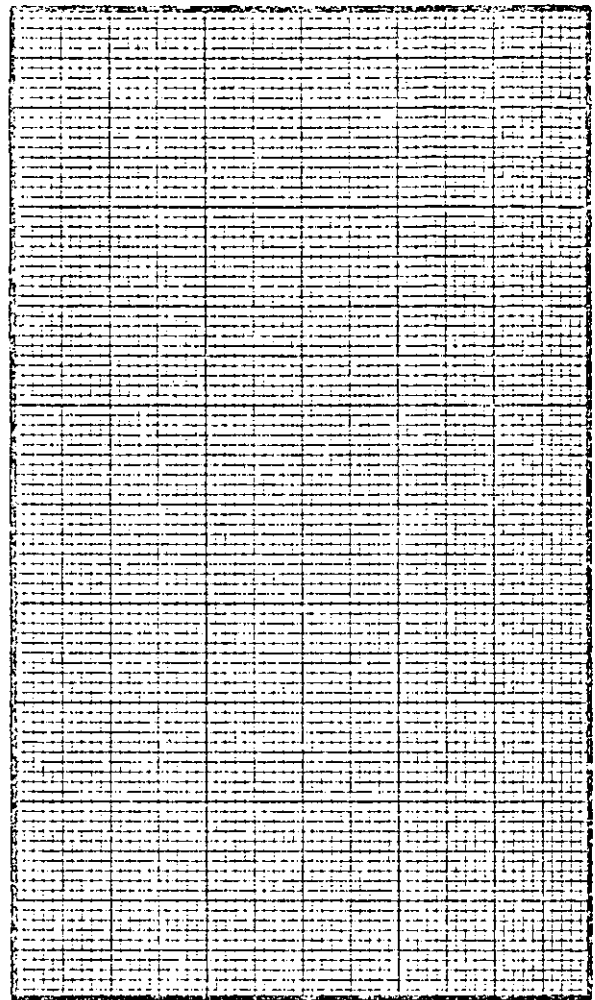


DIAGRAM OF STACK, PORTS, & TRAVERSE
POINTS (indicate direction of flow)

INSIDE DIMENSIONS OF SAMPLE PLANE

STACK GAUGE PRESSURE in. H₂O _____

NEAREST UPSTREAM DISTURBANCE _____

NEAREST DOWNSTREAM DISTURBANCE _____

PROCESS & CONTROL EQUIPMENT
DESCRIPTION _____



SCOTT ENVIRONMENTAL TECHNOLOGY, INC.

MOISTURE

WIMPINGERS

FINAL VOLUME 264 ml
INITIAL VOLUME 200 ml
NET VOLUME 64 ml

SILICA GEL

FINAL WEIGHT 475.9 g
INITIAL WEIGHT 477.1 g
NET WEIGHT 1.2 g
TOTAL MOISTURE 73 %

ANALYTICAL DATA BY _____

ACETONE FRONT WASH

FINAL 155.9637 146.3640 mg
TARE 86.0816 89.0254 mg
NET 69.8821 57.3386 mg

FILTER NUMBER 1

FINAL 7055 mg
TARE 3848 mg
NET 3207 mg

FILTER NUMBER 2

FINAL 12754 114 1014 mg
TARE _____ mg
NET _____ mg

FILTER NUMBER 3

FINAL _____ mg
TARE _____ mg
NET _____ mg

CYCLONE

FINAL _____ mg
TARE _____ mg
NET _____ mg

TOTAL FRONT

_____ mg

ACETONE BACK WASH

FINAL _____ mg
TARE _____ mg
NET _____ mg

ETHER-CHLOROFORM EXTRACT

FINAL _____ mg
TARE _____ mg
NET _____ mg

WATER EVAPORATION

FINAL _____ mg
TARE _____ mg
NET _____ mg

TOTAL BACK

_____ mg

I CERTIFY THAT THE SAMPLES DESCRIBED
BY THIS DATA SHEET WERE COLLECTED IN
ACCORDANCE WITH METHODS OUTLINED BY

I FURTHER CERTIFY THAT THE SAMPLES
WERE IN THE POSSESSION OF, OR SEALED
FOR SHIPMENT BY COMMON CARRIER BY,
MYSELF UNTIL DELIVERY TO A LABORATORY
FOR ANALYSIS.

SIGNED _____ DATE _____
WITNESS _____ DATE _____
I CERTIFY THAT I RECEIVED THE SAMPLES
DESCRIBED BY THIS DATA SHEET FROM THE
ABOVE NAMED INDIVIDUAL AND ANALYZED
THEM IN ACCORDANCE WITH THE ABOVE
METHOD.

NOMOGRAPH DATA BY _____

CALIBRATED PRESSURE DIFFERENTIAL ACROSS ORIFICE, in. H ₂ O	ΔH_0	
AVERAGE METER TEMPERATURE (AMBIENT + 20°F), °F	$T_{m,avg}$	
PERCENT MOISTURE IN GAS STREAM BY VOLUME	R_{wo}	
BAROMETRIC PRESSURE AT METER, in. Hg	P_m	
STATIC PRESSURE IN STACK, in. Hg		
$P_m \pm 0.013 \times$ STACK GAUGE PRESSURE in in. H ₂ O	P_s	
RATIO OF STATIC PRESSURE TO METER PRESSURE	P_s/P_m	
AVERAGE STACK TEMPERATURE, °F	$T_{s,avg}$	
AVERAGE VELOCITY HEAD, in. H ₂ O	ΔP_{avg}	
MAXIMUM VELOCITY HEAD, in. H ₂ O	ΔP_{max}	
C FACTOR		
CALCULATED NOZZLE DIAMETER, in.		
ACTUAL NOZZLE DIAMETER, in.		
REFERENCE ΔP , in. H ₂ O		

DRY MOLECULAR WEIGHT DETERMINATION BY _____

SAMPLING TIME (24-hr CLOCK) _____

SAMPLING LOCATION _____

SAMPLE TYPE (BAG, INTEGRATED, CONTINUOUS) _____

ANALYTICAL METHOD _____

AMBIENT TEMPERATURE _____

RUN GAS	1		2		3		AVERAGE NET VOLUME
	ACTUAL READING	NET	ACTUAL READING	NET	ACTUAL READING	NET	
CO ₂	99.6	0.4					
O ₂ (NET IS ACTUAL O ₂ READING MINUS ACTUAL CO ₂ READING)	78.6	21.0					
CO (NET IS ACTUAL CO READING MINUS ACTUAL O ₂ READING)		78.6					

TEST NUMBER

SCALE WITH GAGE



SCOTT ENVIRONMENTAL TECHNOLOGY, INC.

PLANT CHEVRON CORP - PICHARD

DATE 12-2-78

PROBE LENGTH & TYPE 2' CULVERS

FYRITE ANALYSIS

CO₂ 0₂

SAMPLING LOCATION OUTLET FROM VENT

ANALYST SCOTT

SAMPLE TYPE METHOD 5

METER BOX NUMBER C SAN R 1.065

RUN NUMBER 04111 #2

PROBE HEATER SETTING

OPERATORS JP -- JPR

FILTER HEATER SETTING

AMBIENT TEMPERATURE 56 (a) 16.45

REFERENCE ΔP 1.10

BAROMETER 30.25

READ AND RECORD ALL DATA EVERY 4 MINUTES

START TIME 1705

TRAVERSE POINT NUMBER	SAMPLING TIME, min	CLOCK TIME (24 hr CLOCK)	GAS METER READING (V, ft ³)	VELOCITY HEAD (ΔP), in. H ₂ O	ORIFICE PRESSURE DIFFERENTIAL (ΔH), in. H ₂ O		STACK TEMPERATURE (T _s), °F	DRY GAS METER TEMPERATURE		PUMP VACUUM, in. Hg	IR PINGER TEMPERATURE, °F	COMMENTS
					DESIRED	ACTUAL		INLET (T _{m in}), °F	OUTLET (T _{m out}), °F			
			INITIAL: 359.163									
1	4		361.330	.53	1.0	1.0	111	67	60	2.0		PROBE 127
2	8		373.355	.57	.98	.98	111	68	60	2.0		PROBE 127
3	12		365.310	.53	.90	.90	111	68	60	2.0		PROBE 127
4	16		367.280	.53	.90	.90	111	70	65	2.0		PROBE 127
5	20		369.330	.53	1.11	1.2	112	78	65	2.3		PROBE 127
6	24		371.577	.53	1.00	1.1	113	80	67	2.1		PROBE 127
7	28		373.930	.71	1.23	1.23	111	85	78	2.3		PROBE 127
8	32		376.235	.91	1.55	1.55	111	85	70	2.8		PROBE 127
9	36		378.630	.79	1.35	1.35	112	97	72	2.7		PROBE 127
10	40		381.510	1.3	2.2	2.2	112	95	75	4.0		PROBE 127
11	44		384.580	1.3	2.2	2.2	112	97	75	4.0		PROBE 127
12	48		387.480	1.1	1.25	1.25	112	100	75	3.5		PROBE 127
13	52		390.333	1.05	1.00	1.00	112	100	75	3.5		PROBE 127
14	56		393.120	.98	1.73	1.73	113	100	77	5.0		PROBE 127
15	60		395.948	1.05	1.80	1.80	112	102	78	3.4		PROBE 127
16	64		398.590	.88	1.53	1.53	112	101	79	3.7		PROBE 127
17	8	1217	401.205	1.2	2.0	2.0	112	93	76	3.3		PROBE 127
18	12		403.995	1.05	1.80	1.80	112	94	78	3.5		PROBE 127
19	16		406.935	1.0	2.0	2.0	112	94	78	3.5		PROBE 127

1.175 in 22500
CLOSE @ 10"
OK

TRAVERSE POINT NUMBER	CLOCK TIME (24-hr CLOCK)		GAS METER READING (V _m), ft ³	VELOCITY HEAD (v _p), in. H ₂ O	ORIFICE PRESSURE DIFFERENTIAL		STACK TEMPERATURE (T _s), °F	DRY GAS METER TEMPERATURE		PUMP VACUUM, in. Hg	IMPINGER TEMPERATURE, °F	COMMENTS
	SAMPLING TIME, min				DESIRED	ACTUAL		INLET	OUTLET			
20	20		429.890	1.2	2.0	2.0	111	100	80	3.8		BOX 294 P100E 153
21	24		412.005	1.4	2.22	2.22	111	102	81	4.2		BOX 294 P100E 153
22	28		416.100	1.5	2.45	2.45	111	104	81	4.2		BOX 294 P100E 151
23	32		420.500	1.5	2.30	2.30	111	105	81	4.2		
24	36		421.980	1.4	2.22	2.22	111	108	82	4.1		BOX 294 P100E 149
25	40		425.135	1.4	2.22	2.22	111	109	83	4.2		200 OK
26	44		429.100	1.4	2.22	2.22	111	110	85	4.0		BOX 294 P100E 151
27	48		432.265	1.3	2.0	2.0	112	110	87	4.0		BOX 294 P100E 151
28	52		435.230	1.1	1.85	1.85	111	110	87	3.8		BOX 294 P100E 151
29	56		438.168	1.2	2.0	2.0	111	110	87	3.7		BOX 294 P100E 150
30	60		441.248	1.3	2.20	2.20	111	110	90	4.0		BOX 294 P100E 148
31	64		444.154	1.1	1.85	1.85	111	110	90	3.9		200 OK
32	68		447.087	1.2	2.0	2.0	111	110	80	3.8		BOX 294 P100E 145
				1.01		1.76	111		80.87			
			87.924	1.04		1.71	571		547			

TRAVERSE POINT LOCATION & VELOCITY DATA BY

TRAVERSE POINT NUMBER	A=FRACTION OF I.D.	R=A×I.D. ID=	C=B+NIPPLE NIPPLE=	VELOCITY HEAD (Δp_s), in. H ₂ O	STACK TEMPERATURE (T_s), °F
1					
2					
3					
4					
5					
6					
7					
8					
9					
10					
11					
12					
13					
14					
15					
16					
17					
18					
19					
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37					
38					
39					
40					
41					
42					
43					
44					
45					
46					
47					
48					
AVERAGE					

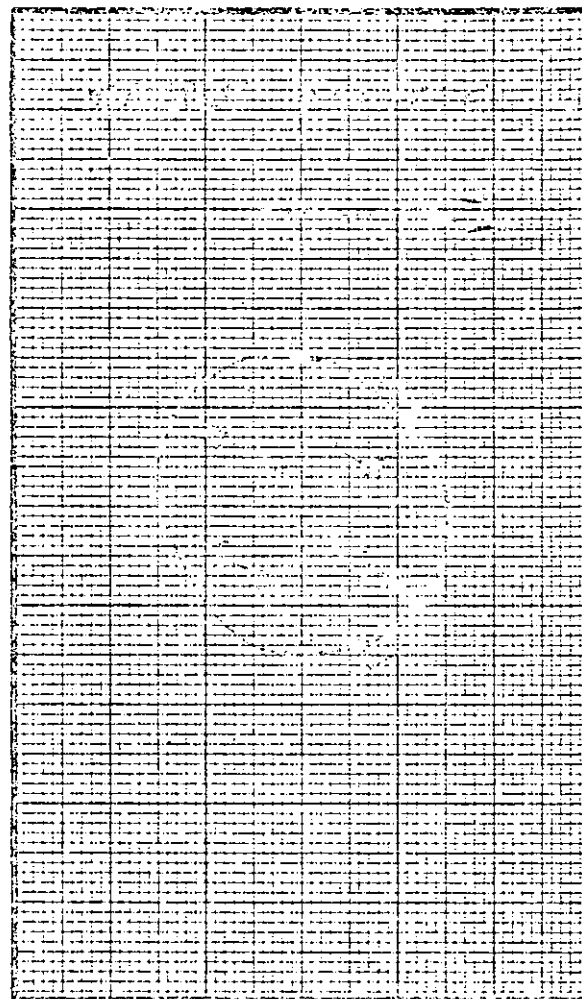


DIAGRAM OF STACK, PORTS, & TRAVERSE
POINTS (indicate direction of flow)

INSIDE DIMENSIONS OF SAMPLE PLANE

STACK GAUGE PRESSURE in. H₂O +1.0

NEAREST UPSTREAM DISTURBANCE _____
NEAREST DOWNSTREAM DISTURBANCE _____

PROCESS & CONTROL EQUIPMENT
DESCRIPTION _____



SCOTT ENVIRONMENTAL TECHNOLOGY, INC.

WIPINGERS

FINAL VOLUME	3/4	ml
INITIAL VOLUME	200	ml
NET VOLUME	1/4	ml

15

743-178

15111

ANALYTICAL DATA

ACETONE FRONT WASH

FINAL	91.5812	mg
TARE	91.3011	mg
NET	2.2801	mg

FILTER NUMBER 1

FINAL	.4358	mg
TARE	.4228	mg
NET	.0130	mg

FILTER NUMBER 2

FINAL	<u>310.1</u>	<u>total</u>	mg
TARE	<u> </u>		mg
NET	<u> </u>		mg

FILTER NUMBER 3

FINAL _____ mg
TARE _____ mg
NET _____ mg

CYCLONE

FINAL	_____ mg
TARE	_____ mg
NET	_____ mg
TOTAL FRONT	_____ mg

SILICA GEL

FINAL WEIGHT	304.4
INITIAL WEIGHT	365.7
NET WEIGHT	36.7
TOTAL MOISTURE	151

ACETONE BACK WASH

FINAL _____ mg
TARE _____ mg
NET _____ mg

ETHER-CHLOROFORM EXTRACT

FINAL _____ mg
TARE _____ mg
NET _____ mg

WATER EVAPORATION

FINAL _____ mg
TARE _____ mg
NET _____ mg

TOTAL BACK

I CERTIFY THAT THE SAMPLES DESCRIBED BY THIS DATA SHEET WERE COLLECTED IN ACCORDANCE WITH METHODS OUTLINED BY

I FURTHER CERTIFY THAT THE SAMPLES WERE IN THE POSSESSION OF, OR SEALED FOR SHIPMENT BY COMMON CARRIER BY, MYSELF UNTIL DELIVERY TO A LABORATORY FOR ANALYSIS.

SIGNED _____ DATE _____
WITNESS _____ DATE _____
I CERTIFY THAT I RECEIVED THE SAMPLES
DESCRIBED BY THIS DATA SHEET FROM THE
ABOVE NAMED INDIVIDUAL AND ANALYZED
THEM IN ACCORDANCE WITH THE ABOVE
BY _____

NOMOGRAPH DATA BY J P

CALIBRATED PRESSURE DIFFERENTIAL ACROSS ORIFICE, in. H ₂ O	ΔH_g	1.865
AVERAGE METER TEMPERATURE (AMBIENT + 20 °F), °F	$T_{m\text{ avg.}}$	80
PERCENT MOISTURE IN GAS STREAM BY VOLUME	B_{w0}	10
BAROMETRIC PRESSURE AT METER, in. Hg	P_m	30.25
STATIC PRESSURE IN STACK, in. Hg $P_m \pm 0.073 \times \text{STACK GAUGE PRESSURE in in. H}_2\text{O}$	P_s	+1.00
RATIO OF STATIC PRESSURE TO METER PRESSURE	P_s/P_m	>1
AVERAGE STACK TEMPERATURE, °F	$T_{s\text{ avg.}}$	116
AVERAGE VELOCITY HEAD, in. H ₂ O	$\Delta P_{\text{avg.}}$	
MAXIMUM VELOCITY HEAD, in. H ₂ O	$\Delta P_{\text{max.}}$	
C FACTOR		9
CALCULATED NOZZLE DIAMETER, in.		
ACTUAL NOZZLE DIAMETER, in.		
REFERENCE Δp , in. H ₂ O		1.1

DRY MOLECULAR WEIGHT DETERMINATION

SAMPLING TIME (24-hr CLOCK)

SAMPLING LOCATION 2000

SAMPLE TYPE (BAG, INTEGRATED, CONTINUOUS)

ANALYTICAL METHOD

AMBIENT TEMPERATURE

RUN GAS	1		2		3		AVERAGE NET VOLUME
	ACTUAL READING	NET	ACTUAL READING	NET	ACTUAL READING	NET	
CO ₂	99.8						12
O ₂ NET IS ACTUAL O ₂ READING MINUS ACTUAL CO ₂ READING	79.2						20.6
CO NET IS ACTUAL CO READING MINUS ACTUAL O ₂ READING						N ₂	79.2

PLANT

ALUMINUM OXIDE

PROBE LENGTH & TYPE

6' GALVANIZED

DATE

12/12/79

NOZZLE I.D.

1.930

SAMPLING LOCATION

INLET AREA 2.14

SAMPLE TYPE

METHODS

METER BOX NUMBER

4001000000

METER BOX NUMBER

4001000000

1.930 ΔH

RUN NUMBER

13

PROBE HEATER SETTING

2200°

OPERATORS

T. S. JAIN

FILTER HEATER SETTING

2200°

AMBIENT TEMPERATURE

51°

REFERENCE ΔP

53

BAROMETER

30.25

READ AND RECORD ALL DATA EVERY

2.5

MINUTES

TRAVERSE POINT NUMBER	SAMPLING TIME, min	CLOCK TIME (24 hr CLOCK)	GAS METER READING (V _m), ft ³	VELOCITY HEAD (ΔP), in. H ₂ O	ORIFICE PRESSURE DIFFERENTIAL (ΔH), in. H ₂ O		STACK TEMPERATURE (T _s), °F	DRY GAS METER TEMPERATURE		PUMP VACUUM, in. Hg	IMPIRDER TEMPERATURE, °F	COMMENTS
					DESIRED	ACTUAL		INLET (T _{m in}), °F	OUTLET (T _{m out}), °F			
			INITIAL: 793.081									
1	1.5		793.081	.15	.10	.10	173	71	69	2.5	50	RECEIVE 2200°
2	5.0		794.253	.23	.73	.73	174	71	68	3.0	50	
3	7.5		795.425	.21	.67	.67	173	72	69	3.5	50	
4	10.0		796.722	.25	.8	.8	173	71	70	4.0	48	
5	12.5		798.110	.30	.83	.83	174	71	71	5.0	48	
6	15.0		799.215	.15	.49	.49	170	72	71	3.5	48	
7	17.5		800.102	.10	.33	.33	169	71	70	2.5	48	
8	20.0		800.874	.03	.21	.21	169	62	70	2.2	48	
9	22.5		801.723	.13	.43	.43	166	60	70	2.8	43	
10	25.0		802.766	.15	.49	.49	166	65	70	3.0	42	
11	27.5		803.909	.20	.45	.45	171	64	71	3.0	40	
12	30.0	31.5440.805.323	805.147	.23	.73	.73	175	67	73	4.1	40	Stop 805.323
13	32.5		807.429	.03	.10	.10	166			11.0	37	Revised 800.852
14	35.0		807.925	.05	.17	.17	174	70	70	1.0	54	
15	37.5		809.277	.15	.40	.40	173	70	70	2.2	50	
16	40.0		809.8	.10	.33	.33	172	73	70	2.2	53	
17	42.5		810.5	.10	.30	.30	171	73	70	2.3	52	
18	45.0		811.647	.10	.30	.30	170	73	72	2.2	52	
19	47.5											

[illegible]

"", Leak rate @ end of test

Vol.	AH	Rate, cfm
6.2	.61	.10 / 11.9 sec.
		13.1
		11.9
		12.5

10	1.0	.10 / 9.8 sec.
		9.5 sec.
		10.1
		10.0

15	1.25	.10 / 7.5 sec.
----	------	----------------

5	.46	.10 / 15 sec
		15 sec
		15.6 sec

3	.20	.10 / 22.9
		20.9
		22.7
		21.2

TRAVERSE POINT LOCATION & VELOCITY DATA

BY _____

TRAVERSE POINT NUMBER	A=FRACTION OF I.D.	B=A x I.D. ID=	C=B+NIPPLE NIPPLE=	VELOCITY HEAD (Δp_s) , in. H ₂ O	STACK TEMPERATURE (T_s) , °F
1					
2					
3					
4					
5					
6					
7					
8					
9					
10					
11					
12					
13					
14					
15					
16					
17					
18					
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41					
42					
43					
44					
45					
46					
47					
48					
AVERAGE					

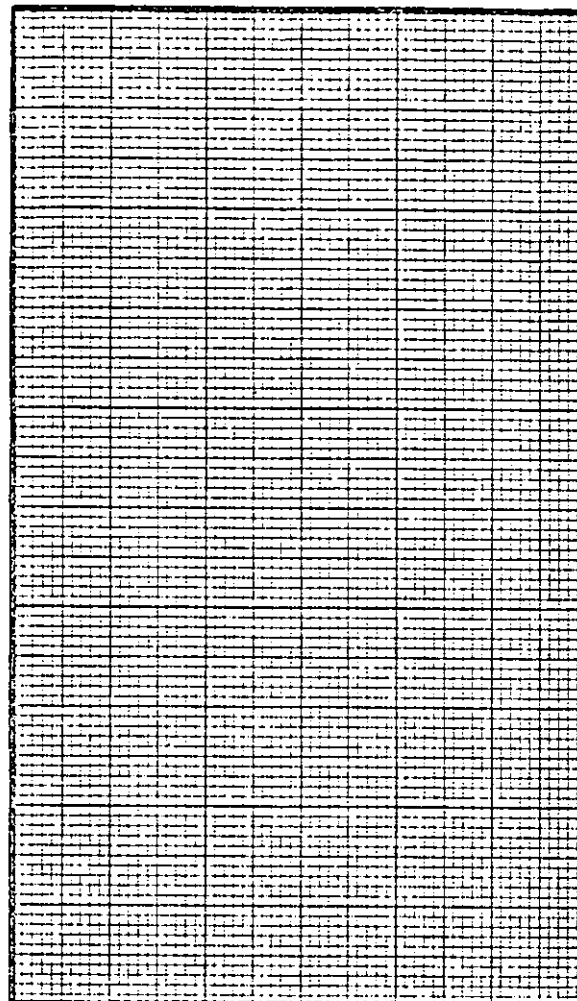


DIAGRAM OF STACK, PORTS, & TRAVERSE POINTS (indicate direction of flow)

INSIDE DIMENSIONS OF SAMPLE PLANE

STACK GAUGE PRESSURE in. H₂O _____

NEAREST UPSTREAM DISTURBANCE _____

NEAREST DOWNSTREAM DISTURBANCE _____

PROCESS & CONTROL EQUIPMENT DESCRIPTION _____



SCOTT ENVIRONMENTAL TECHNOLOGY, INC.

MOISTURE

IMPINGERS

FINAL VOLUME 241 ml
INITIAL VOLUME 200 ml
NET VOLUME 41 ml

SILICA GEL

FINAL WEIGHT 451.2 g
INITIAL WEIGHT 455.3 g
NET WEIGHT 4.1 g
TOTAL MOISTURE 56

IMPINGERS

41 22.3 ml
18

2 — A SMALL AMOUNT OF SILICA GEL

ANALYTICAL DATA BY _____

ACETONE FRONT WASH

FINAL 110.000 mg
TARE 79.000 mg
NET 31.000 mg

FILTER NUMBER 1

FINAL 6078 mg
TARE 4251 mg
NET 1827 mg

FILTER NUMBER 2

FINAL 110.000 mg
TARE 79.000 mg
NET 31.000 mg

FILTER NUMBER 3

FINAL mg
TARE mg
NET mg

CYCLONE

FINAL mg
TARE mg
NET mg

TOTAL FRONT mg

ACETONE BACK WASH

FINAL mg
TARE mg
NET mg

ETHER-CHLOROFORM EXTRACT

FINAL mg
TARE mg
NET mg

WATER EVAPORATION

FINAL mg
TARE mg
NET mg

TOTAL BACK mg

I CERTIFY THAT THE SAMPLES DESCRIBED BY THIS DATA SHEET WERE COLLECTED IN ACCORDANCE WITH METHODS OUTLINED BY

I FURTHER CERTIFY THAT THE SAMPLES WERE IN THE POSSESSION OF, OR SEALED FOR SHIPMENT BY COMMON CARRIER BY, MYSELF UNTIL DELIVERY TO A LABORATORY FOR ANALYSIS.

SIGNED _____ DATE _____
WITNESS _____ DATE _____
I CERTIFY THAT I RECEIVED THE SAMPLES DESCRIBED BY THIS DATA SHEET FROM THE ABOVE NAMED INDIVIDUAL AND ANALYZED THEM IN ACCORDANCE WITH THE ABOVE

NOMOGRAPH DATA BY _____

CALIBRATED PRESSURE DIFFERENTIAL ACROSS ORIFICE, in. H ₂ O	ΔH _g	
AVERAGE METER TEMPERATURE (AMBIENT + 20°F), °F	T _{m avg.}	
PERCENT MOISTURE IN GAS STREAM BY VOLUME	B _{W0}	
BAROMETRIC PRESSURE AT METER, in. Hg	P _m	
STATIC PRESSURE IN STACK, in. Hg	P _s	
P _m ± 0.073 x STACK GAUGE PRESSURE (in in. H ₂ O)	P _s /P _m	
RATIO OF STATIC PRESSURE TO METER PRESSURE		
AVERAGE STACK TEMPERATURE, °F	T _{s avg.}	
AVERAGE VELOCITY HEAD, in. H ₂ O	ΔP _{avg.}	
MAXIMUM VELOCITY HEAD, in. H ₂ O	ΔP _{max.}	
C FACTOR		
CALCULATED NOZZLE DIAMETER, in.		
ACTUAL NOZZLE DIAMETER, in.		
REFERENCE ΔP, in. H ₂ O		

DRY MOLECULAR WEIGHT DETERMINATION BY _____

SAMPLING TIME (24-hr CLOCK) _____

SAMPLING LOCATION _____

SAMPLE TYPE (BAG, INTEGRATED, CONTINUOUS) _____

ANALYTICAL METHOD _____

AMBIENT TEMPERATURE _____

RUN GAS	1	2	3	AVERAGE NET VOLUME
	ACTUAL READING	ACTUAL READING	ACTUAL READING	
CO ₂				
O ₂ (NET IS ACTUAL O ₂ READING MINUS ACTUAL CO ₂ READING)				
CO (NET IS ACTUAL CO READING MINUS ACTUAL O ₂ READING)				



FIELD DATA SHEET

PROJECT NUMBER TEST NUMBER PLANT AMMONIACAL RICHMONDPROBE LENGTH & TYPE 2' GAGE

FYRITE ANALYSIS

DATE 12-13-78NOZZLE I.D. 1.210CO₂ O₂SAMPLING LOCATION OUTLETSAMPLE BOX NUMBER 300501SAMPLE TYPE METHODMETER BOX NUMBER SANIT 1.865 A=1075RUN NUMBER OUTLET #3PROBE HEATER SETTING UARMAC @ 11%OPERATORS TR, JLRFILTER HEATER SETTING 11200AMBIENT TEMPERATURE REFERENCE ΔP 1.1READ AND RECORD ALL DATA EVERY 4 MINUTESBAROMETER 10.0
10.0
10.0

TRAVERSE POINT NUMBER	CLOCK TIME SAMPLING TIME, min	GAS METER READING (V _m), ft ³	VELOCITY HEAD (W _g), in. H ₂ O	ORIFICE PRESSURE DIFFERENTIAL (ΔH), in. H ₂ O		STACK TEMPERATURE (T _s), °F	DRY GAS METER TEMPERATURE		PUMP VACUUM, in. Hg	IMPIRGER TEMPERATURE, °F	COMMENTS
				DESIRED	ACTUAL		INLET (T _{m in}), °F	OUTLET (T _{m out}), °F			
1	4	457.768	1.1	1.85	1.85	112	67	64	1.0		BOX 147 PROBE 165
2	8	460.493	1.1	1.85	1.85	111	70	75	1.5		BOX 148 PROBE 165
3	12	463.210	1.1	1.85	1.85	111	72	70	6.5		BOX 147 PROBE 165
4	16	465.927	1.1	1.85	1.85	114	73	75	7.2		BOX 152 PROBE 165
5	20	466.847	1.2	2.0	2.0	115	87	70	8.0		BOX 185 PROBE 165
6	24	471.842	1.2	2.0	2.0	114	93	71	8.0		BOX 183 PROBE 165
7	28	474.656	1.05	1.8	1.9	114	96	74	7.4		BOX 180 PROBE 165
8	32	477.754	1.5	2.5	2.5	113	98	74	10.0		THANK FIRST GAGE LAST READ
9	36	481.003	1.5	2.5	2.5	113	100	74	10.0		BOX 185 PROBE 165
10	40	484.206	1.4	2.35	2.35	114	101	74	9.5		BOX 152 PROBE 165
11	44	487.475	1.6	2.65	2.65	113	103	75	10.8		BOX 155 PROBE 165
12	48	490.640	1.3	2.2	2.2	114	105	76	9.2		BOX 143 PROBE 165
13	52	493.775	1.4	2.45	2.35	113	105	78	9.5		BOX 141 PROBE 165
14	56	498.000	1.2	2.0	2.0	113	105	78	8.2		BOX 142 PROBE 165
15	60	500.892	1.2	2.0	2.0	113	106	79	8.0		BOX 145 PROBE 165
16	64	503.814	1.2	2.0	2.0	114	106	80	8.0		ZERO IS OK
17	68	506.535	1.05	1.8	1.8	115	85	72	7.0		BOX 143 PROBE 182
18	72	509.322	1.1	1.85	1.85	115	86	72	7.5		BOX 141 PROBE 165

[illegible]

TRAVERSE POINT LOCATION & VELOCITY DATA BY

TRAVERSE POINT NUMBER	A=FRACTION OF I.D.	B=AxI.D. ID=	C=B+NIPPLE NIPPLE=	VELOCITY HEAD (Δp_s), in. H ₂ O	STACK TEMPERATURE (T _g), °F
1					
2					
3					
4					
5					
6					
7					
8					
9					
10					
11					
12					
13					
14					
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46					
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48					
AVERAGE					

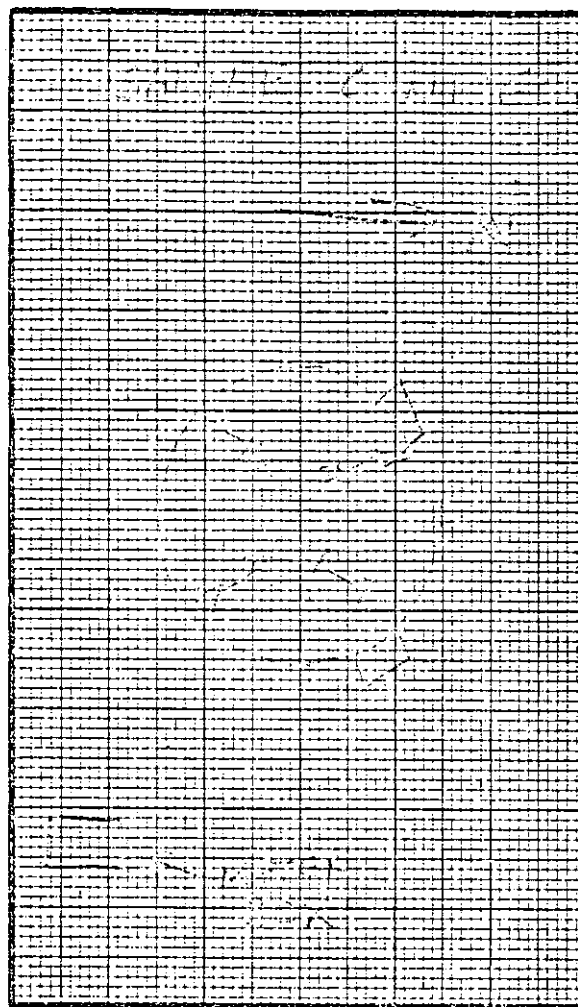


DIAGRAM OF STACK, PORTS, & TRAVERSE
POINTS (indicate direction of flow)

INSIDE DIMENSIONS OF SAMPLE PLANE

STACK GAUGE PRESSURE in. H₂O

NEAREST UPSTREAM DISTURBANCE
NEAREST DOWNSTREAM DISTURBANCE

PROCESS & CONTROL EQUIPMENT
DESCRIPTION



SCOTT ENVIRONMENTAL TECHNOLOGY, INC.

MOISTURE

IMPINGERS

FINAL VOLUME 3.52 ml
INITIAL VOLUME 7.00 ml
NET VOLUME 1.52 ml

SILICA GEL

FINAL WEIGHT 499.6 g
INITIAL WEIGHT 144.0 g
NET WEIGHT 355.6 g
TOTAL MOISTURE 185 g

283
187
165
352

ANALYTICAL DATA BY

ACETONE FRONT WASH

FINAL 90.1474 mg
TARE 59.6571 mg
NET 30.4903 mg

FILTER NUMBER 1

FINAL 14.22 mg
TARE 112.74 mg
NET 3.68 mg

FILTER NUMBER 2

FINAL 825.1 mg
TARE 40.28 mg
NET 784.82 mg

FILTER NUMBER 3

FINAL mg
TARE mg
NET mg

CYCLONE

FINAL mg
TARE mg
NET mg

TOTAL FRONT mg

ACETONE BACK WASH

FINAL mg
TARE mg
NET mg

ETHER-CHLOROFORM EXTRACT

FINAL mg
TARE mg
NET mg

WATER EVAPORATION

FINAL mg
TARE mg
NET mg

TOTAL BACK mg

I CERTIFY THAT THE SAMPLES DESCRIBED BY THIS DATA SHEET WERE COLLECTED IN ACCORDANCE WITH METHODS OUTLINED BY

I FURTHER CERTIFY THAT THE SAMPLES WERE IN THE POSSESSION OF, OR SEALED FOR SHIPMENT BY COMMON CARRIER BY, MYSELF UNTIL DELIVERY TO A LABORATORY FOR ANALYSIS.

SIGNED DATE
WITNESS DATE
I CERTIFY THAT I RECEIVED THE SAMPLES DESCRIBED BY THIS DATA SHEET FROM THE ABOVE NAMED INDIVIDUAL AND ANALYZED THEM IN ACCORDANCE WITH THE ABOVE

NOMOGRAPH DATA BY

CALIBRATED PRESSURE DIFFERENTIAL ACROSS ORIFICE, in. H ₂ O	ΔH_0
AVERAGE METER TEMPERATURE (AMBIENT + 20°F), °F	$T_{m, avg.}$
PERCENT MOISTURE IN GAS STREAM BY VOLUME	B_{mo}
BAROMETRIC PRESSURE AT METER, in. Hg	P_m
STATIC PRESSURE IN STACK, in. Hg	P_s
$P_m \pm 0.073 \times$ STACK GAUGE PRESSURE (in in. H ₂ O)	P_s/P_m
RATIO OF STATIC PRESSURE TO METER PRESSURE	$T_{s, avg.}$
AVERAGE STACK TEMPERATURE, °F	$\Delta P_{avg.}$
AVERAGE VELOCITY HEAD, in. H ₂ O	$\Delta P_{max.}$
MAXIMUM VELOCITY HEAD, in. H ₂ O	
C FACTOR	
CALCULATED NOZZLE DIAMETER, in.	
ACTUAL NOZZLE DIAMETER, in.	
REFERENCE ΔP , in. H ₂ O	

DRY MOLECULAR WEIGHT DETERMINATION BY

SAMPLING TIME (24-hr CLOCK)

SAMPLING LOCATION

SAMPLE TYPE (BAG, INTEGRATED, CONTINUOUS)

ANALYTICAL METHOD

AMBIENT TEMPERATURE

RUN	1		2		3		AVERAGE NET VOLUME
	ACTUAL READING	NET	ACTUAL READING	NET	ACTUAL READING	NET	
GAS							
CO ₂							
O ₂ (NET IS ACTUAL O ₂ READING MINUS ACTUAL CO ₂ READING)							
CO (NET IS ACTUAL CO READING MINUS ACTUAL O ₂ READING)							

PROJECT NUMBER

TEST NUMBER

FIELD DATA SHEET

5



SCOTT ENVIRONMENTAL TECHNOLOGY, INC.

PLANT CHRYSLER DETROITPROBE LENGTH & TYPE 10' 6" 55

FYRITE ANALYSIS

DATE 12/13/78NOZZLE I.D. .750CO₂ O₂SAMPLING LOCATION INLET AFTER DUCTSAMPLE BOX NUMBER SCOTT 5001SAMPLE TYPE IMPACTEDMETER BOX NUMBER SCOTT 5001 1.00RUN NUMBER 1PROBE HEATER SETTING 250°OPERATORS T.S. & W.N.FILTER HEATER SETTING 275°AMBIENT TEMPERATURE 65°REFERENCE ΔP .50

BAROMETER

READ AND RECORD ALL DATA EVERY 2 MINUTES

TRAVERSE POINT NUMBER	SAMPLING TIME, min	CLOCK TIME (24 hr CLOCK)	GAS METER READING (V _m), ft ³	VELOCITY HEAD (ΔP), in. H ₂ O	ORIFICE PRESSURE DIFFERENTIAL (ΔH), in. H ₂ O		STACK TEMPERATURE (T _s), °F	DRYGAS METER TEMPERATURE		PUMP VACUUM, in. Hg	IMPINGER TEMPERATURE, °F	COMMENTS
					DESIRED	ACTUAL		INLET (T _{m in}), °F	OUTLET (T _{m out}), °F			
1	2			.10	.65	.65	173	71	73	2.5		
2	4		853.930	.10	.58	.58	173	75	73	2.3		
3	6		854.728	.12	.33	.33	173	75	74	1.9		
4	8		855.450	.12	.33	.33	174	76	75	1.9		
5	10		856.192	.12	.33	.33	174	79	76	1.9		
6	12		856.989	.15	.49	.49	175	80	77	1.2		
7	14		857.958	.24	.77	.77	177	82	77	2.9		
8	16		859.062	.30	.95	.95	178	81	79	2.2		
9	18		860.281	.38	1.2	1.2	177	83	80	4.0		
10	20		861.632	.40	1.28	1.3	179	83	80	4.2		
11	22		863.010	.45	1.43	1.4	182	91	81	4.5		
12	24		864.487	.49	1.57	1.5	184	93	82	4.5		
13	26		Traverse only	50.47	1.43	1.4	180					Intake air 34.75 in B64.63
14	28			.41			182		510			Nozzle plugged w/soot
15	30		12.511	.35	.53	.53	182					
16	32		12.510	.38			184	171				
17	34			.40			183	171				
18	36			.35			184					
19	38			.45			183					

TRAVERSE POINT LOCATION & VELOCITY DATA BY

TRAVERSE POINT NUMBER	A=FRACTION OF I.D.	B=AxI.D. ID=	C=B+NIPPLE NIPPLE=	VELOCITY HEAD (Δp_s), in.H ₂ O	STACK TEMPERATURE (T_s), °F
1					
2					
3					
4					
5					
6					
7					
8					
9					
10					
11					
12					
13					
14					
15					
16					
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48					
AVERAGE					

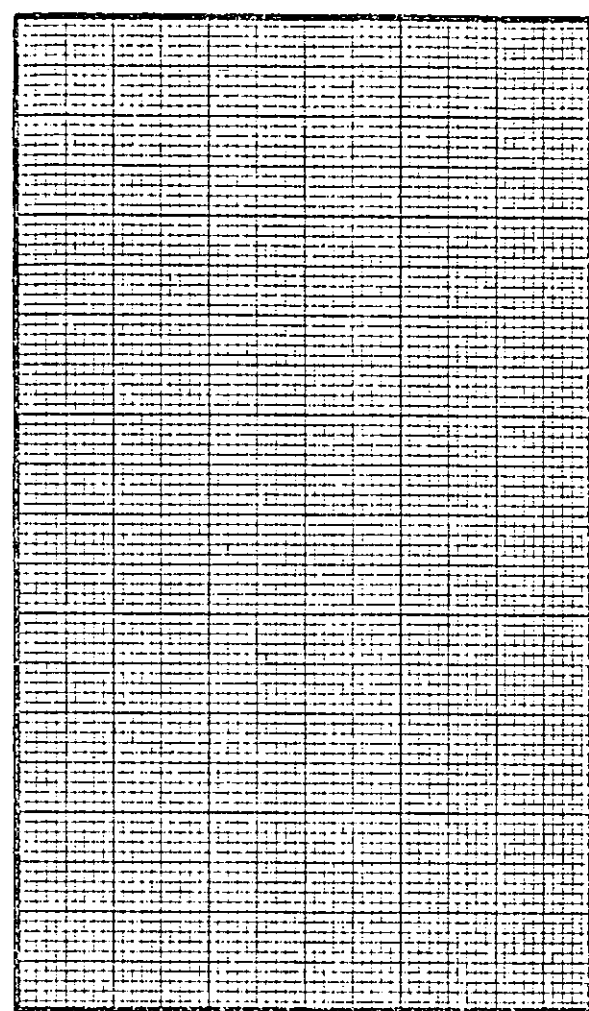


DIAGRAM OF STACK, PORTS, & TRAVERSE
 POINTS (indicate direction of flow)

INSIDE DIMENSIONS OF SAMPLE PLANE

STACK GAUGE PRESSURE in. H₂O

NEAREST UPSTREAM DISTURBANCE
 NEAREST DOWNSTREAM DISTURBANCE

PROCESS & CONTROL EQUIPMENT
 DESCRIPTION



SCOTT ENVIRONMENTAL TECHNOLOGY, INC.

MOISTURE

DRIPPINGS

FINAL VOLUME 212 ml
INITIAL VOLUME 200 ml
NET VOLUME 12 ml

SILICA GEL

FINAL WEIGHT 471.9 g
INITIAL WEIGHT 467.7 g
NET WEIGHT 4.2 g
TOTAL MOISTURE 16 %

ANALYTICAL DATA BY _____

ACETONE FRONT WASH

FINAL 116.1234 mg
TARE 826.000 mg
NET 31.5774 mg

FILTER NUMBER 1

FINAL 14367 mg
TARE 42.99 mg
NET 96.8 mg

FILTER NUMBER 2

FINAL 31351.2 mg
TARE _____ mg
NET _____ mg

FILTER NUMBER 3

FINAL _____ mg
TARE _____ mg
NET _____ mg

CYCLONE

FINAL _____ mg
TARE _____ mg
NET _____ mg

TOTAL FRONT _____ mg

ACETONE BACK WASH

FINAL _____ mg
TARE _____ mg
NET _____ mg

ETHER-CHLOROFORM EXTRACT

FINAL _____ mg
TARE _____ mg
NET _____ mg

WATER EVAPORATION

FINAL _____ mg
TARE _____ mg
NET _____ mg
TOTAL BACK _____ mg

I CERTIFY THAT THE SAMPLES DESCRIBED BY THIS DATA SHEET WERE COLLECTED IN ACCORDANCE WITH METHODS OUTLINED BY _____

I FURTHER CERTIFY THAT THE SAMPLES WERE IN THE POSSESSION OF, OR SEALED FOR SHIPMENT BY COMMON CARRIER BY, MYSELF UNTIL DELIVERY TO A LABORATORY FOR ANALYSIS.

SIGNED _____ DATE _____
WITNESS _____ DATE _____
I CERTIFY THAT I RECEIVED THE SAMPLES DESCRIBED BY THIS DATA SHEET FROM THE ABOVE NAMED INDIVIDUAL AND ANALYZED THEM IN ACCORDANCE WITH THE ABOVE METHODS OUTLINED BY _____

NOMOGRAPH DATA BY _____

CALIBRATED PRESSURE DIFFERENTIAL ACROSS ORIFICE, in. H ₂ O	ΔH_0	
AVERAGE METER TEMPERATURE (AMBIENT + 20°F), °F	$T_{m,avg.}$	
PERCENT MOISTURE IN GAS STREAM BY VOLUME	B_{w0}	
BAROMETRIC PRESSURE AT METER, in. Hg	P_m	
STATIC PRESSURE IN STACK, in. Hg		
$P_m \pm 0.073 \times$ STACK GAUGE PRESSURE in in. H ₂ O	P_s	
RATIO OF STATIC PRESSURE TO METER PRESSURE	P_s/P_m	
AVERAGE STACK TEMPERATURE, °F	$T_{s,avg.}$	
AVERAGE VELOCITY HEAD, in. H ₂ O	$\Delta P_{avg.}$	
MAXIMUM VELOCITY HEAD, in. H ₂ O	$\Delta P_{max.}$	
C FACTOR		
CALCULATED NOZZLE DIAMETER, in.		
ACTUAL NOZZLE DIAMETER, in.		
REFERENCE ΔP , in. H ₂ O		

DRY MOLECULAR WEIGHT DETERMINATION BY _____

SAMPLING TIME (24-hr CLOCK) _____
SAMPLING LOCATION _____
SAMPLE TYPE (BAG, INTEGRATED, CONTINUOUS) _____
ANALYTICAL METHOD _____
AMBIENT TEMPERATURE _____

RUN	1		2		3	
	ACTUAL READING	NET	ACTUAL READING	NET	ACTUAL READING	NET
GAS						
CO ₂						
O ₂ (NET IS ACTUAL O ₂ READING MINUS ACTUAL CO ₂ READING)						
CO (NET IS ACTUAL CO READING MINUS ACTUAL O ₂ READING)						

CHEVRON OBTAIN RICHMOND
ANDERSEN STACK SAMPLER DATA

Date: Dec 13th 1978 Test/Run Number: Chevron Outlets, Andersen

Operator: w/ Nunes Meter Box No. Scott San. B. & ΔHa 1.83 Andersen No. Set 2

Grain Loading From 5 gr/dscf Nozzle Size .250
Est. Sampling Time 2.5 min.

Sampling Location & Point Number: Outlet/Inlet, Point 19 (7 of 12 in center part of 3 ports)

Average Velocity Head From 12 Traverse, ΔP_s .25 Average Stack Temp. From 12 Traverse, T_s 178

Flow Setting From Nomograph, ΔH _____ Reference ΔP .58

Time: Start Stop Elapsed
2.0 min.

			<u>In</u>	<u>Out</u>	<u>Avg.</u>
Gas Volume: Final	852.182 cf.	Meter Temp: Final	78	76	
Initial	851.185 cf.	Initial	77	74	<u>76.25</u>
Total	.997 cf. x .44 = .937		155	150	

Stack Velocity Head, ΔP_s .25 Flow Rate, ΔH .67 Stack Temp, T_s 179°F

Moisture From 14 (%) ≈ 8.4% Gas Density From 13 M_g lb/lb-mole

Corrected Volume dscf Corrected Flow Rate dscf/min

Temperature Correction Factor for Aerodynamic Size of Particles
Taken From Andersen Manual, Figure 3

<u>O</u> <u>Plate</u>	<u>31.1832</u> <u>Tare (g)</u>	<u>31.1907</u> <u>Final (g)</u>	<u>TOTAL</u> <u>PLATE & ALUMINUM</u> <u>Net (mg)</u>	<u>7.5 mg.</u> <u>%</u>	<u>Cum. %</u>	<u>ECD</u> <u>(Microns)</u>
1	20.9620	20.9710	.127 *	127. + 7.5 = 22.8 = 157.3		
2	21.8752	21.8983	.7895 *	799.5		
3	22.42235	22.4331	1.27155 *	1271.55		
4	15.36675	15.3711	.41385 *	413.95		
5	11.0634	11.0657	.0712 *	71.2		
6	11.21995	11.2215	.01315 *	13.15		
7	11.2990	11.2995	.0005	0.5		
8	22.2182	22.2182	0.0000	0.0		

Back-Up Filter .18685 .18715 0.0003

Probe & Head Wash 88.1506 88.1734 22.8

* Includes particulate impacted on plate and loose particulate collected on plate and weighed separately in aluminum dish. See next page.



ANDERSEN PARTICLE SIZE ANALYSIS

Total weight for each plate includes particulate impacted on plate and loose particulate collected on plates, but weighed separately in aluminum dishes.

SAMPLE WEIGHTS

CHEVRON ORTHO
RICHMOND

		SET 2		SAMPLE WT.		TOTAL
PLATE NO	TAIRE	AL. DISH	FINAL	(DISH)	(PLATE)	
0						
1	20.9620	1.3255	1.4435	.118.	.009	.127
2	21.8752	1.3206	2.0870	.7664	.0231	.7895
3	22.42235	1.3240	2.5848	1.2608	.01075	1.27155
4	15.36675	1.3205	1.7300	.4095	.00435	.41385
5	11.0634	1.3108	1.3797	.0689	.0023	.0712
6	11.21935	1.3191	1.3307	.0116	.00155	.01315
7	11.2930				.0005	.0005
8	22.2182				0.0	0.0
9						

Ammonium Sulfate Moisture Analysis

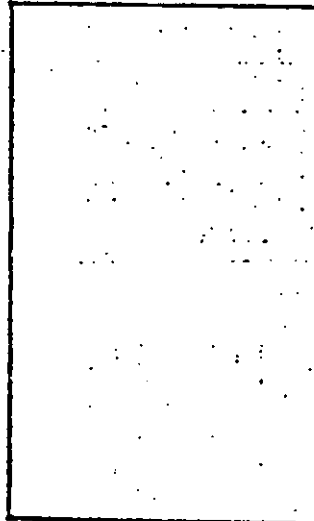
Plant: chevron chemical company

<u>Sample Location</u>	<u>DATE</u>	<u>TIME</u>	<u>Tare wt</u> <u>gms.</u>	<u>Total wt.</u> <u>Wet, gms</u>	<u>Total wt.</u> <u>Dry, gms</u>	<u>Net wt.</u> <u>Wet, gms</u>	<u>Net wt</u> <u>Dry, gms</u>
INLET	12/12	1442	268.2	629.2	627.0	361.0	358.8
OUTLET	12/12	1440	267.3	611.6	611.0	344.3	343.7
INLET	12/12	1712	267.9	640.0	638.1	372.1	370.2
OUTLET	12/12	1711	267.9	654.5	653.5	386.6	385.6
INLET	12/13	1119	267.6	671.7	671.6	409.1	407.0
OUTLET	12/13	1117	268.1	660.4	659.9	392.3	391.8

FIGURE 9-1 RECORD OF VISUAL DETERMINATION OF OPACITY

PAGE 1 of 3

COMPANY CHEVRON ORENO
 LOCATION OUTLET
 TEST NUMBER 1
 DATE 12/12/78
 TYPE FACILITY INHALES (See Description)
 CONTROL DEVICE VENTURURI



HOURS OF OBSERVATION _____
 OBSERVER DBL
 OBSERVER CERTIFICATION DATE 11/1/78
 OBSERVER AFFILIATION SAFETY
 POINT OF EMISSIONS _____
 HEIGHT OF DISCHARGE POINT 20'

CLOCK TIME _____
 OBSERVER LOCATION
 Distance to Discharge _____
 Direction from Discharge _____
 Height of Observation Point _____

BACKGROUND DESCRIPTION

WEATHER CONDITIONS
 Wind Direction _____

Wind Speed _____

Ambient Temperature _____

SKY CONDITIONS (clear, overcast, % clouds, etc.) _____

PLUME DESCRIPTION
 Color _____

Distance Visible _____

OTHER INFORMATION _____

Initial				Final
150'				150'
SE				SE
0'				0'
gray clouds				gray clouds
outlet				outlet
0-5				10-20
50				55
75% clouds				75% clouds
white				white
50'				50'

SUMMARY OF AVERAGE OPACITY

Set Number	Time Start--End	Opacity	
		Sum	Average
1	11:30 - 1:30		0.7

Readings ranged from 0 to 10 % opacity

The source was/was not in compliance with _____ at the time evaluation was made.

FIGURE 9-2 OBSERVATION RECORD

PAGE 2 OF 3

COMPANY CHEVRON OILFIELD
 LOCATION ORANGE
 TEST NUMBER 1
 DATE 12/12/75

OBSERVER DK
 TYPE FACILITY WATER GUM
 POINT OF EMISSIONS 2 WEST

Hr.	Min.	Seconds					STEAM PLUME (check if applicable)		COMMENTS
		0	15	30	45		Attached	Detached	
	0	0	0	0	0				
	1	0	0	0	0				
	2	0	0	0	0				
	3	0	0	0	0				
	4	0	0	0	0				
	5	0	0	0	0				
	6	0	0	0	0				
	7	0	0	0	0				
	8	0	0	0	0				
	9	0	0	0	0				
	10	0	0	0	0				
	11	0	0	0	0				
	12	0	0	0	0				
	13	0	0	0	0				
	14	0	0	0	0				
	15	0	0	0	0				
	16	0	0	0	0				
	17	0	0	0	0				
	18	0	0	0	0				
	19	0	0	0	0				
	20	0	0	0	0				
	21	0	0	0	0				
	22	0	0	0	0				
	23	0	0	0	0				
	24	0	0	0	0				
	25	0	0	0	0				
	26	0	0	0	0				
	27	0	0	0	0				
	28	0	0	0	0				
	29	0	0	0	0				

Start
12:30
PM

Stop
12:42
PM

FIGURE 9-2 OBSERVATION RECORD
(Continued)

PAGE 2 OF 3

COMPANY CHEVRON OILFIELD
 LOCATION ORANGE
 TEST NUMBER 1
 DATE 12/12/75

OBSERVER DK
 TYPE FACILITY WATER GUM
 POINT OF EMISSIONS 2 WEST

Hr.	Min.	Seconds					STEAM PLUME (check if applicable)		COMMENTS
		0	15	30	45		Attached	Detached	
	30	0	0	0	0				
	31	0	0	0	0				
	32	0	0	0	0				
	33	0	0	0	0				
	34	0	0	0	0				
	35	0	0	0	0				
	36	0	0	0	0				
	37	0	0	0	0				
	38	0	0	0	0				
	39	0	0	0	0				
	40	0	0	0	0				
	41	0	0	0	0				
	42	0	0	0	0				
	43	0	0	0	0				
	44	0	0	0	0				
	45	0	0	0	0				
	46	0	0	0	0				
	47	0	0	0	0				
	48	0	0	0	0				
	49	0	0	0	0				
	50	0	0	0	0				
	51	0	0	0	0				
	52	0	0	0	0				
	53	0	0	0	0				
	54	0	0	0	0				
	55	0	0	0	0				
	56	0	0	0	0				
	57	0	0	0	0				
	58	0	0	0	0				
	59	0	0	0	0				

[FR Doc. 74-33163 Filed 11-11-74; 8:48 am]

FIGURE 9-2 OBSERVATION RECORD

PAGE 3 OF 3

COMPANY Calvin and Opus
LOCATION OUTLET
TEST NUMBER 1
DATE 12-12-75

OBSERVER DK
TYPE FACILITY _____
POINT OF EMISSIONS _____

Hr.	Min.	Seconds					STEAM PLUME (check if applicable)		COMMENTS
		0	15	30	45	60	Attached	Detached	
	0	5	0	0	0	0			
	1	0	0	0	0	0			
	2	0	0	0	0	0			
	3	0	0	0	0	0			
	4	0	0	0	0	0			
	5	0	0	0	0	0			
	6	0	0	0	0	0			
	7	0	0	0	0	0			
	8	0	0	0	0	0			
	9	0	0	0	0	0			
	10	0	0	0	0	0			
	11	0	0	0	0	0			
	12	0	0	0	0	0			
	13	0	0	0	0	0			
	14	0	0	0	0	0			
	15	0	0	0	0	0			
	16	0	0	0	0	0			
	17	0	0	0	0	0			
	18	0	0	0	0	0			
	19	0	0	0	0	0			
	20	0	0	0	0	0			
	21	0	0	0	0	0			
	22	0	0	0	0	0			
	23	0	0	0	0	0			
	24	0	0	0	0	0			
	25	0	0	0	0	0			
	26	0	0	0	0	0			
	27	0	0	0	0	0			
	28	0	0	0	0	0			
	29	0	0	0	0	0			

Atty: 010

FIGURE 9-2 OBSERVATION RECORD
(Continued)

PAGE 3 OF 3

COMPANY Calvin and Opus
LOCATION OUTLET
TEST NUMBER 1
DATE 12-12-75

OBSERVER DK
TYPE FACILITY _____
POINT OF EMISSIONS _____

Hr.	Min.	Seconds					STEAM PLUME (check if applicable)		COMMENTS
		0	15	30	45	60	Attached	Detached	
	30	0	0	0	0	0			
	31	0	0	0	0	0			
	32	0	0	0	0	0			
	33	0	0	0	0	0			
	34	0	0	0	0	0			
	35	0	0	0	0	0			
	36	0	0	0	0	0			
	37	0	0	0	0	0			
	38	0	0	0	0	0			
	39	0	0	0	0	0			
	40	0	0	0	0	0			
	41	0	0	0	0	0			
	42	0	0	0	0	0			
	43	0	0	0	0	0			
	44	0	0	0	0	0			
	45	0	0	0	0	0			
	46	0	0	0	0	0			
	47	0	0	0	0	0			
	48	0	0	0	0	0			
	49	0	0	0	0	0			
	50	0	0	0	0	0			
	51	0	0	0	0	0			
	52	0	0	0	0	0			
	53	0	0	0	0	0			
	54	0	0	0	0	0			
	55	0	0	0	0	0			
	56	0	0	0	0	0			
	57	0	0	0	0	0			
	58	0	0	0	0	0			
	59	0	0	0	0	0			

FIGURE 9-1

[illegible]

HOURS OF OBSERVATION _____
OBSERVER DK
OBSERVER CERTIFICATION DATE 10/1/78
OBSERVER AFFILIATION SEA
POINT OF EMISSIONS _____
HEIGHT OF DISCHARGE POINT 20'

CLOCK TIME

OBSERVER LOCATION

Distance to Discharge

Direction from Discharge.

Height of Observation Point

BACKGROUND DESCRIPTION

WEATHER CONDITIONS

Wind Direction

Wind Speed

Ambient Temperature

SKY CONDITIONS (clear, overcast, & clouds, etc.)

PLUME DESCRIPTION

Color

Distance Visible

OTHER INFORMATION

Initial			Final
150'			150'
SE			SE
0'			0'
75' clouds			75' clouds
100'			100'
75'			50'
75' clouds			75' clouds
white			white
50'			50'

SUMMARY OF AVERAGE OPACITY

[illegible]

Readings ranged from ___ to ___ % opacity.

The source was/was not 'in compliance with _____ at the time evaluation was made.

FIGURE 9-2 OBSERVATION RECORD

PAGE 2 OF 3

COMPANY Coleman
LOCATION 1000
TEST NUMBER 1000
DATE 12/12/78

OBSERVER DR
TYPE FACILITY 1000
POINT OF EMISSIONS 1000

Hr.	Min.	Seconds				STEAM PLUME (check if applicable)		COMMENTS
		0	15	30	45	Attached	Detached	
	0	0	0	0	0			
	1	0	0	0	0			
	2	0	0	0	0			
	3	0	0	0	0			
	4	0	0	0	0			
	5	0	0	0	0			
	6	0	0	0	0			
	7	0	0	0	0			
	8	0	0	0	0			
	9	0	0	0	0			
	10	0	0	0	0			
	11	0	0	0	0			
	12	0	0	0	0			
	13	0	0	0	0			
	14	0	0	0	0			
	15	0	0	0	0			
	16	0	0	0	0			
	17	0	0	0	0			
	18	0	0	0	0			
	19	0	0	0	0			
	20	0	0	0	0			
	21	0	0	0	0			
	22	0	0	0	0			
	23	0	0	0	0			
	24	0	0	0	0			
	25	0	0	0	0			
	26	0	0	0	0			
	27	0	0	0	0			
	28	0	0	0	0			
	29	0	0	0	0			

FIGURE 9-2 OBSERVATION RECORD
(Continued)

PAGE 2 OF 3

COMPANY Coleman
LOCATION 1000
TEST NUMBER 1000
DATE 12/12/78

OBSERVER DR
TYPE FACILITY 1000
POINT OF EMISSIONS 1000

Hr.	Min.	Seconds				STEAM PLUME (check if applicable)		COMMENTS
		0	15	30	45	Attached	Detached	
	30	0	0	0	0			
	31	0	0	0	0			
	32	0	0	0	0			
	33	0	0	0	0			
	34	0	0	0	0			
	35	0	0	0	0			
	36	0	0	0	0			
	37	0	0	0	0			
	38	0	0	0	0			
	39	0	0	0	0			
	40	0	0	0	0			
	41	0	0	0	0			
	42	0	0	0	0			
	43	0	0	0	0			
	44	0	0	0	0			
	45	0	0	0	0			
	46	0	0	0	0			
	47	0	0	0	0			
	48	0	0	0	0			
	49	0	0	0	0			
	50	0	0	0	0			
	51	0	0	0	0			
	52	0	0	0	0			
	53	0	0	0	0			
	54	0	0	0	0			
	55	0	0	0	0			
	56	0	0	0	0			
	57	0	0	0	0			
	58	0	0	0	0			
	59	0	0	0	0			

[FR Doc. 74-23150 Filed 11-11-74; 8:43 am]

FIGURE 9-2 OBSERVATION RECORD

PAGE 3 OF 3

COMPANY CHEVRON OIL CO
LOCATION OIL FIELD
TEST NUMBER 2
DATE 12/12/78

OBSERVER DK
TYPE FACILITY
POINT OF EMISSIONS

FIGURE 9-2 OBSERVATION RECORD
(Continued)

PAGE 3 OF 3

COMPANY CHEVRON OIL CO
LOCATION OIL FIELD
TEST NUMBER 2
DATE 12/12/78

OBSERVER DK
TYPE FACILITY
POINT OF EMISSIONS

Hr.	Min.	Seconds					STEAM PLUME (check if applicable)		COMMENTS
		0	15	30	45		Attached	Detached	
	0	0	0	0	0				
	1	0	0	0	0				
	2	0	0	0	0				
	3	0	0	0	0				
	4	0	0	0	0				
	5	0	0	0	0				
	6	0	0	0	0				
	7	0	0	0	0				
	8	0	0	0	0				
	9	0	0	0	0				
	10	0	0	0	0				
	11	0	0	0	0				
	12	0	0	0	0				
	13	0	0	0	0				
	14	0	0	0	0				
	15	0	0	0	0				
	16	0	0	0	0				
	17	0	0	0	0				
	18	0	0	0	0				
	19	0	0	0	0				
	20	0	0	0	0				
	21	0	0	0	0				
	22	0	0	0	0				
	23	0	0	0	0				
	24	0	0	0	0				
	25	0	0	0	0				
	26	0	0	0	0				
	27	0	0	0	0				
	28	0	0	0	0				
	29	0	0	0	0				

Aug = 0.1°

Hr.	Min.	Seconds					STEAM PLUME (check if applicable)		COMMENTS
		0	15	30	45		Attached	Detached	
	30								
	31								
	32								
	33								
	34								
	35								
	36								
	37								
	38								
	39								
	40								
	41								
	42								
	43								
	44								
	45								
	46								
	47								
	48								
	49								
	50								
	51								
	52								
	53								
	54								
	55								
	56								
	57								
	58								
	59								

[FR Doc. 74-28180 Filed 11-11-74; 8:43 am]

FIGURE 9-5

PAGE 1 OF 4

COMPANY CHRYSLER CREDIT CORP

LOCATION	DISTRICT

TEST NUMBER 3

DATE 12/13/11

TYPE FACILITY *Medical, S.D. problem*

CONTROL DEVICE 100

HOURS OF OBSERVATION

OBSERVER *DK*

OBSERVER CERTIFICATION DATE 12/1/78

OBSERVER AFFILIATION

POINT OF EMISSIONS

HEIGHT OF DISCHARGE POINT 20'

Initial			Final
150'			150'
SE			SE
0'			0'
Blue Sky white clouds			Blue Sky white clouds
0-5			0-10
over S			over S
50			55
50-60			50-60 + 500
white			white
50'			50'

CLOCK TIME

OBSERVER LOCATION

Distance to Discharge

Direction from Discharge.

Height of Observation Point

BACKGROUND DESCRIPTION

WEATHER CONDITIONS

Wind Direction

Wind Speed

Ambient Temperature

SKY CONDITIONS (clear, overcast, % clouds, etc.)

PLUME DESCRIPTION

Color

Distance Visible

OTHER INFORMATION

SUMMARY OF AVERAGE OPACITY

[illegible]

Readings ranged from _____ to _____ % opacity.

The source was/was not in compliance with _____ at the time evaluation was made.

FIGURE 9-2 OBSERVATION RECORD

PAGE 2 OF 4

COMPANY CHEVRON OILFIELD
LOCATION 001-101
TEST NUMBER 2
DATE 12/18/78

OBSERVER DK
TYPE FACILITY WELL
POINT OF EMISSIONS WELL

Hr.	Min.	Seconds					STEAM PLUME		COMMENTS
		0	15	30	45	60	(check if applicable)	Detached	
	0	0	0	0	0	0	✓		
	1	0	0	0	0	0			
	2	0	0	0	0	0			
	3	0	0	0	0	0			
	4	0	0	0	0	0			
	5	0	0	0	0	0			
	6	0	0	0	0	0			
	7	0	0	0	0	0			
	8	0	0	0	0	0			
	9	0	0	0	0	0			
	10	0	0	0	0	0			
	11	0	0	0	0	0			
	12	0	0	0	0	0			
	13	0	0	0	0	0			
	14	0	0	0	0	0			
	15	0	0	0	0	0			
	16	0	0	0	0	0			
	17	0	0	0	0	0			
	18	0	0	0	0	0			
	19	0	0	0	0	0			
	20	0	0	0	0	0			
	21	0	0	0	0	0			
	22	0	0	0	0	0			
	23	0	0	0	0	0			
	24	0	0	0	0	0			
	25	0	0	0	0	0			
	26	0	0	0	0	0			
	27	0	0	0	0	0			
	28	0	0	0	0	0			
	29	0	0	0	0	0			

Shift
8:46
met (w/and)
(RWD)
outlet
(RWD)

FIGURE 9-2 OBSERVATION RECORD (Continued)

PAGE 2 OF 4

COMPANY CHEVRON OILFIELD
LOCATION 001-101
TEST NUMBER 2
DATE 12/18/78

OBSERVER DK
TYPE FACILITY WELL
POINT OF EMISSIONS WELL

Hr.	Min.	Seconds					STEAM PLUME		COMMENTS
		0	15	30	45	60	(check if applicable)	Detached	
	30	0	0	0	0	0	✓		
	31	0	0	0	0	0			
	32	0	0	0	0	0			
	33	0	0	0	0	0			
	34	0	0	0	0	0			
	35	0	0	0	0	0			
	36	0	0	0	0	0			
	37	0	0	0	0	0			
	38	0	0	0	0	0			
	39	0	0	0	0	0			
	40	0	0	0	0	0			
	41	0	0	0	0	0			
	42	0	0	0	0	0			
	43	0	0	0	0	0			
	44	0	0	0	0	0			
	45	0	0	0	0	0			
	46	0	0	0	0	0			
	47	0	0	0	0	0			
	48	0	0	0	0	0			
	49	0	0	0	0	0			
	50	0	0	0	0	0			
	51	0	0	0	0	0			
	52	0	0	0	0	0			
	53	0	0	0	0	0			
	54	0	0	0	0	0			
	55	0	0	0	0	0			
	56	0	0	0	0	0			
	57	0	0	0	0	0			
	58	0	0	0	0	0			
	59	0	0	0	0	0			

[PR Doc 74-20150 Filed 11-11-74; 8:46 am]

FIGURE 9-2 OBSERVATION RECORD

COMPANY CHEVRON OILFIELD
 LOCATION ORLANDO
 TEST NUMBER 101111
 DATE 12/15/78
 OBSERVER DR
 TYPE FACILITY POINT OF EMISSIONS

FIGURE 9-2 OBSERVATION RECORD
 (Continued)

COMPANY CHEVRON OILFIELD
 LOCATION ORLANDO
 TEST NUMBER 101111
 DATE 12/15/78
 OBSERVER DK
 TYPE FACILITY POINT OF EMISSIONS

Hr.	Min.	Seconds				STEAM PLUME (check if applicable)		COMMENTS
		0	15	30	45	Attached	Detached	
	0	0	0	0	0	✓		
	1	0	0	0	0			
	2	0	0	0	0			
	3	0	0	0	0			
	4	0	0	0	0			
	5	0	0	0	0			
	6	0	0	0	0			
	7	0	0	0	0			
	8	0	0	0	0			
	9	0	0	0	0			
	10	0	0	0	0			
	11	0	0	0	0			
	12	0	0	0	0			
	13	0	0	0	0			
	14	0	0	0	0			
	15	0	0	0	0			
	16	0	0	0	0			
	17	0	0	0	0			
	18	0	0	0	0			
	19	0	0	0	0			
	20	0	0	0	0			
	21	0	0	0	0			
	22	0	0	0	0			
	23	0	0	0	0			
	24	0	0	0	0			
	25	0	0	0	0			
	26	0	0	0	0			
	27	0	0	0	0			
	28	0	0	0	0			
	29	0	0	0	0			

Hr.	Min.	Seconds				STEAM PLUME (check if applicable)		COMMENTS
		0	15	30	45	Attached	Detached	
	30	0	0	0	0	✓		
	31	0	0	0	0			
	32	0	0	0	0			
	33	0	0	0	0			
	34	0	0	0	0			
	35	0	0	0	0			
	36	0	0	0	0			
	37	0	0	0	0			
	38	0	0	0	0			
	39	0	0	0	0			
	40	0	0	0	0			
	41	0	0	0	0			
	42	0	0	0	0			
	43	0	0	0	0			
	44	0	0	0	0			
	45	0	0	0	0			
	46	0	0	0	0			
	47	0	0	0	0			
	48	0	0	0	0			
	49	0	0	0	0			
	50	0	0	0	0			
	51	0	0	0	0			
	52	0	0	0	0			
	53	0	0	0	0			
	54	0	0	0	0			
	55	0	0	0	0			
	56	0	0	0	0			
	57	0	0	0	0			
	58	0	0	0	0			
	59	0	0	0	0			

FIGURE 9-2 OBSERVATION RECORD

PAGE 4 OF 4

COMPANY CHEVRON ORTHO
 LOCATION 00111
 TEST NUMBER 50
 DATE 12/15/75

OBSERVER DK
 TYPE FACILITY INDUSTRIAL SO₂
 POINT OF EMISSIONS

Hr.	Min.	Seconds					STEAM PLUME (check if applicable)		COMMENTS
		0	15	30	45	60	Attached	Detached	
1	0	0	0	0	0	0			
2	0	0	0	0	0	0			
3	0	0	0	0	0	0			
4	0	0	0	0	0	0			
5	0	0	0	0	0	0			
6	0	0	0	0	0	0			
7	0	0	0	0	0	0			
8	0	0	0	0	0	0			
9	0	0	0	0	0	0			
10	0	0	0	0	0	0			
11	0	0	0	0	0	0			
12	0	0	0	0	0	0			
13	0	0	0	0	0	0			
14	0	0	0	0	0	0			
15	0	0	0	0	0	0			
16	0	0	0	0	0	0			
17	0	0	0	0	0	0			
18	0	0	0	0	0	0			
19	0	0	0	0	0	0			
20	0	0	0	0	0	0			
21	0	0	0	0	0	0			
22	0	0	0	0	0	0			
23	0	0	0	0	0	0			
24	0	0	0	0	0	0			
25	0	0	0	0	0	0			
26	0	0	0	0	0	0			
27	0	0	0	0	0	0			
28	0	0	0	0	0	0			
29	0	0	0	0	0	0			

Aug = 0/6

FIGURE 9-2 OBSERVATION RECORD
 (Continued)

PAGE 4 OF 4

COMPANY CHEVRON ORTHO
 LOCATION 00111
 TEST NUMBER 50
 DATE 12/15/75

OBSERVER DK
 TYPE FACILITY
 POINT OF EMISSIONS

Start 11:55 AM (to finish in 4 hours)

Hr.	Min.	Seconds					STEAM PLUME (check if applicable)		COMMENTS
		0	15	30	45	60	Attached	Detached	
30	0	0	0	0	0	0			
31	0	0	0	0	0	0			
32	0	0	0	0	0	0			
33	0	0	0	0	0	0			
34	0	0	0	0	0	0			
35	0	0	0	0	0	0			
36	0	0	0	0	0	0			
37	0	0	0	0	0	0			
38	0	0	0	0	0	0			
39	0	0	0	0	0	0			
40	0	0	0	0	0	0			
41	0	0	0	0	0	0			
42	0	0	0	0	0	0			
43	0	0	0	0	0	0			
44	0	0	0	0	0	0			
45	0	0	0	0	0	0			
46	0	0	0	0	0	0			
47	0	0	0	0	0	0			
48	0	0	0	0	0	0			
49	0	0	0	0	0	0			
50	0	0	0	0	0	0			
51	0	0	0	0	0	0			
52	0	0	0	0	0	0			
53	0	0	0	0	0	0			
54	0	0	0	0	0	0			
55	0	0	0	0	0	0			
56	0	0	0	0	0	0			
57	0	0	0	0	0	0			
58	0	0	0	0	0	0			
59	0	0	0	0	0	0			

[FR Doc. 74-20159 Filed 11-11-74; 8:58 am]

28 Nov

stopped at 11:45 AM due to clear sky

FIGURE 9-9

PAGE 1 of 2

1. The first step is to identify the problem or question that needs to be addressed. This involves understanding the context and the specific requirements of the task.

2. Next, it is important to gather relevant information and resources. This may involve researching existing solutions, consulting with experts, or collecting data.

3. Once the information is gathered, the next step is to analyze it and identify the key factors that influence the outcome. This often involves breaking down the problem into smaller, more manageable parts.

4. After analysis, a plan should be developed that outlines the steps to be taken to solve the problem. This plan should be flexible enough to allow for adjustments as more information becomes available.

5. The final step is to implement the plan and monitor the progress. This involves putting the plan into action and regularly checking in to see how things are going. If necessary, adjustments should be made along the way.

HOURS OF OBSERVATION

OBSERVER

OBSERVER CERTIFICATION DATE 12/1/78

OBSERVER AFFILIATION

POINT OF EMISSIONS

HEIGHT OF DISCHARGE POINT 20'

CLOCK TIME

OBSERVER LOCATION

Distance to Discharge

Direction from Discharge

Height of Observation Point

BACKGROUND DESCRIPTION

WEATHER CONDITIONS

Wind Direction

Wind Speed

Ambient Temperature

SKY CONDITIONS (clear, overcast, & clouds, etc.)

PLUME DESCRIPTION

Color

Distance Visible

OTHER INFORMATION

Initial			Final
150'			
SE			
0'			
Shovel Blow 14			
Shovel Blow 55			
0-15			
55			
dent rod			
white			
50'			

SUMMARY OF AVERAGE OPACITY

[illegible]

Readings ranged from	to	% opacity
0.00	0.05	0.00
0.05	0.10	0.05
0.10	0.15	0.10
0.15	0.20	0.15
0.20	0.25	0.20
0.25	0.30	0.25
0.30	0.35	0.30
0.35	0.40	0.35
0.40	0.45	0.40
0.45	0.50	0.45
0.50	0.55	0.50
0.55	0.60	0.55
0.60	0.65	0.60
0.65	0.70	0.65
0.70	0.75	0.70
0.75	0.80	0.75
0.80	0.85	0.80
0.85	0.90	0.85
0.90	0.95	0.90
0.95	1.00	0.95

The source was/was not 'in compliance with _____ at the time evaluation was made.

FIGURE 9-2 OBSERVATION RECORD

PAGE 2 OF 2

COMPANY Champion OBSERVER DK
 LOCATION 000000 TYPE FACILITY 000000
 TEST NUMBER 4 POINT OF EMISSIONS
 DATE 12/13/88

Hr.	Min.	Seconds					STEAM PLUME (check if applicable)		COMMENTS
		0	15	30	45	59	Attached	Detached	
	0	1	0	1					Start time of observation
	1	0	1	1					End time of observation
	2	0	1	1					10.0000000000
	3	0	1	1					10.0000000000
	4	0	1	1					10.0000000000
	5	0	1	1					
	6	0	1	1					
	7	0	1	1					
	8	0	1	1					
	9	0	1	1					
	10	0	1	1					
	11	0	1	1					
	12	0	1	1					
	13	0	1	1					
	14	0	1	1					
	15	0	1	1					
	16	0	1	1					
	17	0	1	1					
	18	0	1	1					
	19	0	1	1					
	20	0	1	1					
	21	0	1	1					
	22	0	1	1					
	23	0	1	1					
	24	0	1	1					
	25	0	1	1					
	26								
	27								
	28								
	29								

Start
2:37
(INLET
REGION
0.42)

Stop
(2:42)

Aug. = 0.1

FIGURE 9-2 OBSERVATION RECORD
(Continued)

PAGE 2 OF 2

COMPANY Champion OBSERVER DK
 LOCATION 000000 TYPE FACILITY 000000
 TEST NUMBER 4 POINT OF EMISSIONS
 DATE 12/13/88

Hr.	Min.	Seconds					STEAM PLUME (check if applicable)		COMMENTS
		0	15	30	45	59	Attached	Detached	
	30								
	31								
	32								
	33								
	34								
	35								
	36								
	37								
	38								
	39								
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[FRT Doc.74-20160 Filed 11-11-74;8:45 am]

APPENDIX B

FIELD DATA SHEETS

TABLE 1

SUMMARY OF AMMONIUM SULFATE PRODUCTION RATE DATA

	Test No.		
	1	2	3
Average Sulfuric Acid Consumption gpm	15.1	15.1	15
Average Ammonia Consumption Lb/Hr	3950	3900	3850
AS Production Based on Sulfuric Acid Consumption, TPD (gpm x 14.7)	222	222	222
AS Production Based on Ammonia Consumption, TPD (Lb/Hr x .0465)	184	181	177
Nominal Plant AS Capacity, TPD	220	220	220

TABLE 2

PROCESS PARAMETERS MONITORED DURING TEST NO. 1

Elapsed Time, Min	0	30	60	90	120	150
Sulfuric Acid Flow, gpm	15.1	15.3	15.0	15.0	15.0	15.0
Ammonia Flow, Lb/Hr	4000	4000	4000	4000	3900	3900
Centrifuge Amperes	21	21	21	20.5	20.2	20.0
Crystallizer Operation:						
Magma Level						
(scale reading)	5	5	5	5	5	5
Vacuum, psia	7	7	7	7	7	7
Magma temperature (°F)	143	142	140	136	136	136
AS Slurry Sp. Gr. Leaving						
Crystallizer (meter)	1.445	1.443	1.442	1.440	1.440	1.440
Percent Free Acid in						
Crystallizer						
Elutriation Leg	.285	.257	.190	.190	.100	.119
Rotary Dryer Temperatures:						
Inlet Gas (°F)	515	510	520	500	500	500
Outlet Gas (°F)	187	187	187	185	188	189
AS Product (°F)	185	185	185	184	185	186
Slurry Surge Tank Level, ft.	5.8	5.6	5.6	5.4	5.6	5.8
AS Product Weigh Belt Rate						
TPH	5.8	5.8	5.8	5.5	5.0	4.3

TABLE 3

PROCESS PARAMETERS MONITORED DURING TEST NO. 2

Elapsed Time, Min	0	30	60	90	120	150	180	210
Sulfuric Acid Flow, gpm	15.0	15.2	15.1	15.1	15.1	15.1	15.1	15.2
Ammonia Flow, lb/Hr.	3900	3900	3900	3900	3900	3900	3900	4000
Centrifuge Amperes	20.2	19	19	19.5	20	20	20	20
Crystallizer Operation:								
Magma Level (scale reading)	5	5	5	5	5	5	5	5
Vacuum, psia	7	7	7	7	7	7	7	7
Magma Temperature, °F	136	140	143	144	145	146	146	148
AS Slurry Sp. Gr. Leaving Crystallizer (meter)	1.440	1.440	1.440	1.440	1.437	1.443	1.444	1.442
Percent Free Acid in Crystallizer Elutriation Leg	.138	.152	.171	.200	.200	.228	.209	.242
Rotary Dryer Temperatures:								
Inlet Gas (°F)	500	500	490	490	490	490	500	510
Outlet Gas (°F)	190	190	190	187	188	188	188	188
AS Product (°F)	187	187	189	185	188	188	188	188
Slurry Surge Tank Level, ft.	6.1	6.4	6.9	7.4	7.7	7.8	7.8	8.6
AS Product Weigh Belt Rate, TPH	4.0	3.1	3.0	2.8	2.9	3.0	3.0	3.0
AS Slurry Feed to Centrifuge Pump Speed RPM*	700	550	550	550	550	550	550	490

*This was recorded to show effect on AS product rate - the latter indicated by weigh belt reading. Normal slurry pump speed is 800 RPM.

TABLE 4

PROCESS PARAMETERS MONITORED DURING TEST NO. 3

Elapsed Time, Min	0	30	60	90	120	150
Sulfuric Acid Flow, gpm	15	15	15	15	15	15
Ammonia Flow, lb/hr	3700	3800	3800	3800	3700	3700
Centrifuge Amperes	21	21	20.5	20.5	20.5	20.5
Crystallizer Operation:						
Magma Level						
(scale reading)	5	5	5	5	5	5
Vacuum, psia	7	7	7	7	7	7
Magma Temperature, °F	148	148	149	150	152	147
AS Slurry Sp. Gr. Leaving Crystallizer (meter)	1.470	1.465	1.462	1.460	1.457	1.445
Percent Free Acid in Crystallizer Elutriation Leg	.138	.162	.142	.119	.190	.190
Rotary Dryer Temperatures:						
Inlet Gas (°F)	510	520	515	510	500	490
Outlet Gas (°F)	185	185	190	188	185	187
AS Product (°F)	185	185	190	187	185	186
Slurry Surge Tank Level Ft.	8.9	8.8	8.6	8.2	7.7	7.1
AS Product Weigh Belt Rate, TPH	5.6	5.7	5.7	5.7	5.7	5.3

United States
Environmental Protection
Agency

Office of Air, Noise, and Radiation
Office of Air Quality Planning and Standards,
Research Triangle Park, NC 27711

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