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AP-42 Section	9.7
Reference	13
Report Sect.	4
Reference	5

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MAY 28 1991

Environmental Health

**ECKLEY ENGINEERING**  
255 North Fulton Street  
Fresno, Ca. 9301  
Attn: Bob Eckley

**SOURCE EMISSION TESTING**

~~HANFORD GROWERS~~

Total Particulate  
PM-10 Particulate  
December 3 & 4, 1990  
*County Line Gin*

Prepared By:

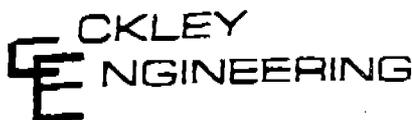
**BTC ENVIRONMENTAL, INC.**  
1536 Eastman Avenue  
Ventura, CA 93003

Job Number  
5019

Laboratory Report Number  
290-188

Test Team Leader  
Cameron Doonahco

Results Verified By:  
Tom Porter - Director Air Test Division



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SJVUAPCD/Kings  
330 Campus Drive  
Hanford, California 93230

RE: County Line Gin, Inc.  
Authority to Construct and Emissions Reduction Credit  
Supplement to May 26, 1991, Application #  
Corrections to Pre-Modification (12/04/90) Source Testing

The attached sheets document errors in the calculation of the pounds per bale pre-modification figures.

One error was caused by multiplying the emissions per cyclone by four cyclones, instead of the correct factor of six, in the #2 Drying System.

The second error was caused by the source testing laboratory's erroneously labeling a 28" diameter candy cane as measuring only 19" in diameter. BTC has provided the attached corrected pages to be incorporated into the original (12/04/90) report to replace the defective pages.

The corrected figures are incorporated into the computation of the 3.21 pounds/bale TSP, as shown on the attached spread sheet.



COUNTY LINE GIN: PRE-MODIFICATION EMISSIONS

EMISSIONS POINT	REFERENCE	TEST DATE	TESTED G/DSCP	TESTED LB/HR	CYCLOPS COLLECTORS (NUMBER & SIZE ("))	BALES/HOUR	SYSTEM ( POUNDS/HOUR)	SYSTEM ( POUNDS/BALE)	
SUCTION	County Line	12/90	0.0378	1.21	4/34	21.9	4.84	0.22	
#1 DRYING	County Line	12/90	0.0596	1.68	6/38	18.4	10.08	0.55	
#2 DRYING	Stratford	12/90	0.0925	4.21	6/38	21.4	<del>16.84</del> 25.26	<del>0.79</del> 1.18	Multiplicat + rather than
NOTES	County Line	12/90	0.1000	<del>4.13</del> 3.96	2/60	18.2	<del>8.26</del> 17.92	<del>0.45</del> 0.98	Lab error see encl as pages
LINT CLEANER	County Line	12/90	0.0601	<del>2.63</del> 1.68	16/38	18.5	26.88	1.45	wrong
OVERFLOW	%(#2 Drying)	12/90	-	-	1/40	-	-	0.20	
G.S. TRASH	Stratford	11/90	0.0357	1.52	2/38	12.7	3.80 adj.	0.30	
BC SCRNSKT	AP-42	-	-	-	-	-	-	0.19	
NOTE CLEANER	%(Notes)	12/90	-	-	1/43	-	-	<del>0.33</del> 0.74	See Notes Note above

Calculated pounds per bale before 1991 modifications = 5.81

\*Allowable under Rule 404

A + 50% PM<sub>10</sub> → 2.905 lb. PM<sub>10</sub>/bale

Pre-Mod

Post-Test

## EMISSION SUMMARY

## #1 DRYER CYCLONE

CONSTITUENT	RUN #1	RUN #2	AVERAGE
Total Particulate			
gr/DSCF	0.0343	0.0849	0.0596
lbs/hr	0.98	2.36	1.67
PM-10 Particulate			
+10 $\mu$ (%)	57.9	62.7	60.3
-10 $\mu$ (%)	42.1	37.3	39.7
+10 $\mu$ (lbs/hr)	0.57	1.48	1.02
-10 $\mu$ (lbs/hr)	0.41	0.88	0.65

r re Mod.

~~Post Test~~

## EMISSION SUMMARY

## SUCTION CYCLONE

CONSTITUENT	RUN #1	RUN #2	AVERAGE
<b>Total Particulate</b>			
gr/DSCF	0.0338	0.0417	<b>0.0378</b>
lbs/hr	1.15	1.26	<b>1.21</b>
<b>PM-10 Particulate</b>			
+10 $\mu$ (%)	0.3	0.7	<b>0.5</b>
-10 $\mu$ (%)	99.7	99.3	<b>99.5</b>
+10 $\mu$ (lbs/hr)	0.00	0.01	<b>0.01</b>
-10 $\mu$ (lbs/hr)	1.15	1.25	<b>1.20</b>

Kremod

Post-test

## EMISSION SUMMARY

## LINT TRAP CYCLONE

CONSTITUENT	RUN #1	RUN #2	AVERAGE
Total Particulate			
gr/DSCF	0.0534	0.0667	0.0601
lbs/hr	2.32	2.92	2.62
PM-10 Particulate			
+10 $\mu$ (%)	64.7	54.3	59.5
-10 $\mu$ (%)	35.3	45.7	40.5
+10 $\mu$ (lbs/hr)	1.50	1.59	1.54
-10 $\mu$ (lbs/hr)	0.82	1.33	1.08

Pre-mod  
~~Post-Test~~

## EMISSION SUMMARY

## MOTE CYCLONE

CONSTITUENT	RUN #1	RUN #2	AVERAGE
Total Particulate			
gr/DSCF	0.0458	0.1653	0.1056
lbs/hr	1.91	6.80	4.36
PM-10 Particulate			
+10 $\mu$ (%)	75.7	69.5	72.6
-10 $\mu$ (%)	24.3	30.5	27.4
+10 $\mu$ (lbs/hr)	1.45	4.73	3.09
-10 $\mu$ (lbs/hr)	0.46	2.07	1.27

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**EMISSION SUMMARY**

**MOTE CYCLONE**

<b>CONSTITUENT</b>	<b>RUN #1</b>	<b>RUN #2</b>	<b>AVERAGE</b>
<b>Total Particulate</b>			
gr/DSCF	0.0458	0.1653	<del>0.1056</del>
lbs/hr	1.91	6.80	4.36
<b>PM-10 Particulate</b>			
+10 $\mu$ (%)	75.7	69.5	72.6
-10 $\mu$ (%)	<del>24.3</del>	30.5	<del>27.4</del>
+10 $\mu$ (lbs/hr)	1.45	4.73	<del>3.09</del>
-10 $\mu$ (lbs/hr)	0.46	2.07	<del>1.26</del>

VWAT/02

**EMISSION SUMMARY**

**LINT TRAP CYCLONE**

<b>CONSTITUENT</b>	<b>RUN #1</b>	<b>RUN #2</b>	<b>AVERAGE</b>
<b>Total Particulate</b>			
gr/DSCF	0.0534	0.0667	0.0601
lbs/hr	2.32	2.92	2.62
<b>PM-10 Particulate</b>			
+10 $\mu$ (%)	64.7	54.3	59.5
-10 $\mu$ (%)	35.3	45.7	40.5
+10 $\mu$ (lbs/hr)	1.50	1.59	
-10 $\mu$ (lbs/hr)	0.82	1.33	

**EMISSION SUMMARY**

**SUCTION CYCLONE**

<b>CONSTITUENT</b>	<b>RUN #1</b>	<b>RUN #2</b>	<b>AVERAGE</b>
<b>Total Particulate</b>			
gr/DSCF	0.0338	0.0417	<b>0.0378</b>
lbs/hr	1.15	1.26	<b>1.21</b>
<b>PM-10 Particulate</b>			
+10 $\mu$ (%)	0.3	0.7	<b>0.5</b>
-10 $\mu$ (%)	99.7	99.3	<b>99.5</b>
+10 $\mu$ (lbs/hr)	0.00	0.01	<b>0.01</b>
-10 $\mu$ (lbs/hr)	1.15	1.25	<b>1.20</b>

EMISSION SUMMARY

#1 DRYER CYCLONE

CONSTITUENT	RUN #1	RUN #2	AVERAGE
<b>Total Particulate</b>			
gr/DSCF	0.0343	0.0849	0.0596
lbs/hr	0.98	2.36	1.67
<b>PM-10 Particulate</b>			
+10 $\mu$ (%)	57.9	62.7	60.3
-10 $\mu$ (%)	42.1	37.3	39.7
+10 $\mu$ (lbs/hr)	0.57	1.48	1.02
-10 $\mu$ (lbs/hr)	0.41	0.88	0.65

**I. INTRODUCTION**

## INTRODUCTION

On December 3 & 4, 1990, BTC Environmental performed source emission tests for PM-10 particulate matter and total particulate matter on various cyclones located at the Hanford Growers cotton gin. The gin is located at 12095 2nd Avenue in Hanford, California. The cyclones were designated as #1 Dryer, Mote, Lint Trap and Suction. A candy cane exhaust duct was attached to the cyclone outlet and routed to ground level producing a uniform flow in a vertical position.

The testing was conducted while the plant was operating at normal conditions and production rates.

## SAMPLING AND ANALYTICAL PROCEDURES

STACK GAS ANALYSIS: The stack gas were assumed to be ambient air. The O<sub>2</sub> value was 20.9% and the CO<sub>2</sub> value was 0.05%.

STACK GAS VELOCITY: The stack gas velocity was determined using an "S" type pitot tube connected to an inclined draft gauge or a magnehelic gauge.

The stack temperature was determined using a thermocouple and an indicating pyrometer. The proportion of water was determined gravimetrically and the dry molecular weight of the stack gas determined by E.P.A. Method 3, equation 3-2. Stack velocities were calculated using E.P.A. Method 2, equation 2-9; gas volumetric flow rate was determined by equation 2-10.

PARTICULATE EMISSIONS: Particulates were collected using a Lase Model 31 stack sampler system that conforms to E.P.A. requirements for particulate sampling. The system consists of a heated probe, heated filter, and cooled impingers (see E.P.A. Method 5). After the weight of the particulates on the filter and in the probe is determined, the total dissolved solids in the the impingers is determined and added to the particulate weight in order to comply with APCD regulations. Blanks for the DI water and acetone were analyzed and subtracted from the total particulate weight.

PM-10 PARTICULATE EMISSIONS: Sampling was done isokinetically from each stack at the same time that the total particulate sampling was being done. The sampling was done by using a Gil cascade impactor. The impactor consists of a nozzle, two (2) stages with slotted filters, a final stage containing a backup-filter, heated probe and cooled impingers containing DI water. The nozzle and the two (2) stages represent the +10 $\mu$  fraction. The final stage, heated probe and the impingers represent the -10 $\mu$  fraction.

The weight from each fraction including the filter weights and the rinses are added together to obtain a total weight. The total weight is divided into the weight obtained from each fraction to obtain the percentage for each fraction. The lb/hr values obtained from the total particulate runs were utilized to obtain the lb/hr for the +10 $\mu$  and the -10 $\mu$  fractions.

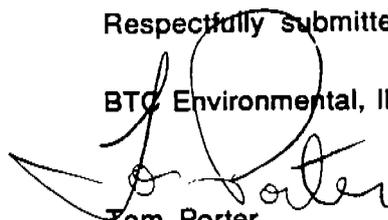
LEAK CHECKS: Leak rates were conducted on the sampling train and the pitot tubes before and after each test. The leak check for the sampling train was done at the nozzle. Any leak rate greater than 0.02 cfm was corrected for in the volume calculations.

All calculations for lb/hr were done by using the flow rate of the stack gas. All values were calculated by using standard conditions (60°F & 29.92 in Hg).

If you have any questions concerning this test or if we can be of further assistance, please contact the undersigned at (805) 644-1095.

Respectfully submitted,

BTC Environmental, INC.



Tom Porter

Director-Air Test Division

Copies: 3 Eckley Attn: Bob Eckley

## **II. WET TEST METHODS DATA SUMMARIES**

METHOD 5 FIELD DATA SUMMARY

MOTE CYCLONE

	Run#1	Run#2
Vlc - Volume of water collected, ml	9.1	6.2
Vm - Gas volume, meter cond., dcf	45.438	38.385
Y - Meter calibration factor	1.023	1.023
Pbar - Barometric pressure, in. Hg	30.21	30.21
Pg - Stack static pressure, in. H2O	30.20	30.20
ΔH - Avg. meter press. diff., in. H2O	1.559	1.569
Tm - Absolute meter temperature, °R	520.9	536.3
Vm(std) - Standard sample gas vol., dscf	47.0334	38.5973
Bws - Water vapor part in gas stream	0.9	0.7
CO2 - Dry concentration, volume %	0.05	0.05
O2 - Dry concentration, volume %	20.9	20.9
Md - Mol wt. stack gas, dry, g/gmole	28.844	28.844
Ms - Mol wt. stack gas, wet, g/gmole	28.747	28.764
Qp - Pitot tube coef., dimensionless	0.850	0.850
Δp - Avg. of sq. roots of each Δp	0.731	0.731
Ts - Absolute stack Temp. °R	520.4	534.3
A - Area of stack, square feet	<sup>4.276</sup> 1.97	<sup>1.97</sup> 4.276
Qstd - Volumetric flow rate, dscfm	4858	4800
An - Area of nozzle, square feet	0.0002712	0.0002712
ø - Sampling time, minutes	72	60
I - Isokinetic variation, percent	95.4	95.1

METHOD 5 FIELD DATA SUMMARY

LINT TRAP CYCLONE

	Run#1	Run#2
Vlc - Volume of water collected, ml	5.5	7.8
Vm - Gas volume, meter cond., dcf	35.530	37.737
Y - Meter calibration factor	1.023	1.023
Pbar - Barometric pressure, in. Hg	30.10	30.10
Pg - Stack static pressure, in. H2O	30.09	30.09
$\Delta H$ - Avg. meter press. diff., in. H2O	0.979	0.999
Tm - Absolute meter temperature, °R	541.6	540.9
Vm(std) - Standard sample gas vol., dscf	35.1947	37.4331
Bws - Water vapor part in gas stream	0.7	1.0
CO2 - Dry concentration, volume %	0.05	0.05
O2 - Dry concentration, volume %	20.9	20.9
Md - Mol wt. stack gas, dry, g/gmole	28.844	28.844
Ms - Mol wt. stack gas, wet, g/gmole	28.766	28.740
Cp - Pitot tube coef., dimensionless	0.850	0.850
$\Delta p$ - Avg. of sq. roots of each $\Delta p$	0.593	0.598
Ts - Absolute stack Temp. °R	565.5	562.4
A - Area of stack, square feet	2.64	2.64
Qstd - Volumetric flow rate, dscfm	5064	5109
An - Area of nozzle, square feet	0.0002712	0.0002712
$\emptyset$ - Sampling time, minutes	72	72
I - Isokinetic variation, percent	91.8	96.8

METHOD 5 FIELD DATA SUMMARY

SUCTION CYCLONE

	Run#1	Run#2
Vlc - Volume of water collected, ml	9.2	9.2
Vm - Gas volume, meter cond., dcf	44.725	37.723
Y - Meter calibration factor	0.969	0.969
Pbar - Barometric pressure, in. Hg	30.27	30.27
Pg - Stack static pressure, in. H2O	30.27	30.27
$\Delta H$ - Avg. meter press. diff., in. H2O	1.434	1.443
Tm - Absolute meter temperature, °R	529.3	536.3
Vm(std) - Standard sample gas vol., dscf	43.2069	35.9649
Bws - Water vapor part in gas stream	1.0	1.2
CO2 - Dry concentration, volume %	0.05	0.05
O2 - Dry concentration, volume %	20.9	20.9
Md - Mol wt. stack gas, dry, g/gmole	28.844	28.844
Ms - Mol wt. stack gas, wet, g/gmole	28.738	28.716
Cp - Pitot tube coef., dimensionless	0.850	0.850
$\Delta p$ - Avg. of sq. roots of each $\Delta p$	0.399	0.404
Ts - Absolute stack Temp. °R	535.5	544.3
A - Area of stack, square feet	2.64	2.64
Qstd - Volumetric flow rate, dscfm	3508	3513
An - Area of nozzle, square feet	0.0004844	0.0004844
$\theta$ - Sampling time, minutes	72	60
I - Isokinetic variation, percent	96.2	96.0

METHOD 5 FIELD DATA SUMMARY

#1 DRYER CYCLONE

	Run#1	Run#2
Vlc - Volume of water collected, ml	14.8	24.1
Vm - Gas volume, meter cond., dcf	44.377	42.250
Y - Meter calibration factor	0.969	0.969
Pbar - Barometric pressure, in. Hg	30.25	30.25
Pg - Stack static pressure, in. H2O	30.25	30.25
$\Delta H$ - Avg. meter press. diff., in. H2O	1.359	1.350
Tm - Absolute meter temperature, °R	539.6	541.0
Vm(std) - Standard sample gas vol., dscf	42.0144	39.8982
Bws - Water vapor part in gas stream	1.6	2.7
CO2 - Dry concentration, volume %	0.05	0.05
O2 - Dry concentration, volume %	20.9	20.9
Md - Mol wt. stack gas, dry, g/gmole	28.844	28.844
Ms - Mol wt. stack gas, wet, g/gmole	28.669	28.548
Cp - Pitot tube coef., dimensionless	0.850	0.850
$\Delta p$ - Avg. of sq. roots of each $\Delta p$	0.537	0.536
Ts - Absolute stack Temp. °R	590.8	606.9
A - Area of stack, square feet	1.97	1.97
Qstd - Volumetric flow rate, dscfm	3333	3250
An - Area of nozzle, square feet	0.0003547	0.0003547
$\emptyset$ - Sampling time, minutes	72	72
I - Isokinetic variation, percent	100.3	97.7

PM-10 FIELD DATA SUMMARY

MOTE CYCLONE

	Run#1	Run#2
Vlc - Volume of water collected, ml	8.0	5.9
Vm - Gas volume, meter cond., dcf	41.340	35.231
Y - Meter calibration factor	0.969	0.969
Pbar - Barometric pressure, in. Hg	30.21	30.21
Pg - Stack static pressure, in. H2O	30.20	30.20
$\Delta H$ - Avg. meter press. diff., in. H2O	1.253	1.252
Tm - Absolute meter temperature, °R	522.7	538.9
Vm(std) - Standard sample gas vol., dscf	40.3391	33.3427
Bws - Water vapor part in gas stream	0.9	0.8
CO2 - Dry concentration, volume %	0.05	0.05
O2 - Dry concentration, volume %	20.9	20.9
Md - Mol wt. stack gas, dry, g/gmole	28.844	28.844
Ms - Mol wt. stack gas, wet, g/gmole	28.745	28.755
Op - Pitot tube coef., dimensionless	0.850	0.850
$\Delta p$ - Avg. of sq. roots of each $\Delta p$	0.731	0.729
Ts - Absolute stack Temp. °R	521.3	534.9
A - Area of stack, square feet	<sup>4.276</sup> 1.97	1.97 <sup>4.276</sup>
Qstd - Volumetric flow rate, dscfm	4853	4782
An - Area of nozzle, square feet	0.0002428	0.0002428
$\theta$ - Sampling time, minutes	72	60
I - Isokinetic variation, percent	96.6	97.3

PM-10 FIELD DATA SUMMARY

LINT TRAP CYCLONE

	Run#1	Run#2
Vlc - Volume of water collected, ml	4.4	7.6
Vm - Gas volume, meter cond. dcf	32.419	33.678
Y - Meter calibration factor	0.969	0.969
Pbar - Barometric pressure, in. Hg	30.10	30.10
Pg - Stack static pressure, in. H2O	30.09	30.09
$\Delta H$ - Avg. meter press. diff., in. H2O	0.804	0.813
Tm - Absolute meter temperature, °R	541.1	540.2
Vm(std) - Standard sample gas vol., dscf	30.4143	31.6498
Bws - Water vapor part in gas stream	0.7	1.1
CO2 - Dry concentration, volume %	0.05	0.05
O2 - Dry concentration, volume %	20.9	20.9
Md - Mol wt. stack gas, dry, g/gmole	28.844	28.844
Ms - Mol wt. stack gas, wet, g/gmole	28.772	28.724
Cp - Pitot tube coef., dimensionless	0.850	0.850
$\Delta p$ - Avg. of sq. roots of each $\Delta p$	0.598	0.602
Ts - Absolute stack Temp. °R	565.5	562.8
A - Area of stack, square feet	2.64	2.64
Qstd - Volumetric flow rate, dscfm	5112	5138
An - Area of nozzle, square feet	0.0002428	0.0002428
$\emptyset$ - Sampling time, minutes	72	72
I - Isokinetic variation, percent	92.7	96.0

**PM-10 FIELD DATA SUMMARY**

**SUCTION CYCLONE**

	Run#1	Run#2
Vlc - Volume of water collected, ml	8.7	6.8
Vm - Gas volume, meter cond., dcf	43.776	36.708
Y - Meter calibration factor	1.023	1.023
Pbar - Barometric pressure, in. Hg	30.27	30.27
Pg - Stack static pressure, in. H2O	30.27	30.27
$\Delta H$ - Avg. meter press. diff., in. H2O	1.432	1.424
Tm - Absolute meter temperature, °R	527.6	531.2
Vm(std) - Standard sample gas vol., dscf	44.8117	37.3222
Bws - Water vapor part in gas stream	0.9	0.8
CO2 - Dry concentration, volume %	0.05	0.05
O2 - Dry concentration, volume %	20.9	20.9
Md - Mol wt. stack gas, dry, g/gmole	28.844	28.844
Ms - Mol wt. stack gas, wet, g/gmole	28.747	28.753
Cp - Pitot tube coef., dimensionless	0.850	0.850
$\Delta p$ - Avg. of sq. roots of each $\Delta p$	0.402	0.404
Ts - Absolute stack Temp. °R	535.5	544.4
A - Area of stack, square feet	2.64	2.64
Qstd - Volumetric flow rate, dscfm	3535	3521
An - Area of nozzle, square feet	0.0004779	0.0004779
$\theta$ - Sampling time, minutes	72	60
I - Isokinetic variation, percent	95.1	95.4

PM-10 FIELD DATA SUMMARY

#1 DRYER CYCLONE

	Run#1	Run#2
Vlc - Volume of water collected, ml	16.7	20.6
Vm - Gas volume, meter cond., dcf	43.153	42.760
Y - Meter calibration factor	1.023	1.023
Pbar - Barometric pressure, in. Hg	30.25	30.25
Pg - Stack static pressure, in. H2O	30.25	30.25
ΔH - Avg. meter press. diff., in. H2O	1.352	1.340
Tm - Absolute meter temperature, °R	537.3	538.7
Vm(std) - Standard sample gas vol., dscf	43.3422	42.8350
Bws - Water vapor part in gas stream	1.8	2.2
CO2 - Dry concentration, volume %	0.05	0.05
O2 - Dry concentration, volume %	20.9	20.9
Md - Mol wt. stack gas, dry, g/gmole	28.844	28.844
Ms - Mol wt. stack gas, wet, g/gmole	28.653	28.607
Cp - Pitot tube coef., dimensionless	0.850	0.850
Δp - Avg. of sq. roots of each Δp	0.536	0.536
Ts - Absolute stack Temp. °R	591.4	607.2
A - Area of stack, square feet	1.97	1.97
Qstd - Volumetric flow rate, dscfm	3321	3266
An - Area of nozzle, square feet	0.0003773	0.0003773
ø - Sampling time, minutes	72	72
I - Isokinetic variation, percent	92.5	93.0

**FIELD DATA & CALCULATIONS SUMMARY**

Client: **Hanford/Eckley**  
 Site: **Hanford Gin**  
 Unit: **Moat**

Date: **12/4/90**  
 Type: **T std = 60 F**  
 Run: **1-Part**

<b>Wlc</b>	Water Condensate Weight	9.1	g		
<b>Vlc</b>	Water Condensate Volume	9.1	ml		
<b>Vm</b>	Metered Sample Gas Volume	45.438	dcf		
<b>Lp</b>	Avg. Leak Rate	0.000	cf		
<b>Vn</b>	Leak Corrected Sample Gas Volume	45.438	dcf		
<b>Y</b>	Dry Gas Meter Calibration Factor	1.023			
<b>Pbar</b>	Barometric Pressure	30.21	In. Hg		
<b>Pg</b>	Static Pressure	-0.15	In. H2O		
<b>Ps</b>	Stack Pressure, Absolute	30.20	in. Hg		
<b>Δ H</b>	Dry Gas Meter Press. Differential, Average	1.559	In. H2O		
<b>Tm</b>	Dry Gas Meter Temperature, Average	60.9	deg. F	520.9	deg. R
<b>Vm(std)</b>	Sample Gas Volume	47.0334	dscf		
<b>Vm(wet)</b>	Sample Gas Volume, Wet	47.4567	scf		
<b>Vw(std)</b>	Water Vapor Volume	0.4233	scf		
<b>Bws</b>	Water Content of Stack Gas	0.009		0.9	%
<b>CO2</b>	Carbon Dioxide, Dry	0.1	%		
<b>O2</b>	Oxygen, Dry	20.9	%		
<b>N2</b>	Nitrogen, Dry	79.1	%		
<b>Md</b>	Molecular Wt. of Stack Gas, Dry	28.844	lb/lb mole		
<b>Ms</b>	Molecular Wt. of Stack Gas, Wet	28.747	lb/lb mole		
<b>Cp</b>	Pitot Calibration Factor	0.850			
<b>Δ P</b>	Velocity Head, Average Square Root	0.731	In. H2O		
<b>Ts</b>	Stack Gas Temperature, Average	60.4	deg. F	520.4	deg. R
<b>As</b>	Area of Stack	1.97	sq ft	19.0	in. dia.
<b>Vs</b>	Stack Gas Velocity	41.14	ft/sec	??	
<b>Qa</b>	Actual Flow Rate	10,555 4.860	cfm		
<b>Qad</b>	Actual Flow Rate, Dry	4.817	dcfm		
<b>Q(std)</b>	Stack Gas Flow Rate	4,858	dscfm		
<b>An</b>	Nozzle Area	0.0002712	sq ft	0.223	in. dia.
<b>Theta</b>	Sampling Time	7.2	min.		
<b>I</b>	Isokinetics	95.4	%		

**FIELD DATA & CALCULATIONS SUMMARY**

Client: **Hanford/Eckley**  
 Site: **Hanford Gln**  
 Unit: **Moat**

Date: **12/4/90**  
 Type: **T std = 60 F**  
 Run: **2-Part**

<b>Wlc</b>	Water Condensate Weight	6.2	g		
<b>Vlc</b>	Water Condensate Volume	6.2	ml		
<b>Vm</b>	Metered Sample Gas Volume	38.385	dcf		
<b>Lp</b>	Avg. Leak Rate	0.000	cf		
<b>Vn</b>	Leak Corrected Sample Gas Volume	38.385	dcf		
<b>Y</b>	Dry Gas Meter Calibration Factor	1.023			
<b>Pbar</b>	Barometric Pressure	30.21	In. Hg		
<b>Pg</b>	Static Pressure	-0.15	In. H2O		
<b>Ps</b>	Stack Pressure, Absolute	30.20	in. Hg		
<b>Δ H</b>	Dry Gas Meter Press. Differential, Average	1.569	In. H2O		
<b>Tm</b>	Dry Gas Meter Temperature, Average	76.3	deg. F	536.3	deg. R
<b>Vm(std)</b>	Sample Gas Volume	38.5973	dscf		
<b>Vm(wet)</b>	Sample Gas Volume, Wet	38.8857	scf		
<b>Vw(std)</b>	Water Vapor Volume	0.2884	scf		
<b>Bws</b>	Water Content of Stack Gas	0.007		0.7	%
<b>CO2</b>	Carbon Dioxide, Dry	0.1	%		
<b>O2</b>	Oxygen, Dry	20.9	%		
<b>N2</b>	Nitrogen, Dry	79.1	%		
<b>Md</b>	Molecular Wt. of Stack Gas, Dry	28.844	lb/lb mole		
<b>Ms</b>	Molecular Wt. of Stack Gas, Wet	28.764	lb/lb mole		
<b>Cp</b>	Pitot Calibration Factor	0.850			
<b>Δ P</b>	Velocity Head, Average Square Root	0.731	In. H2O		
<b>Ts</b>	Stack Gas Temperature, Average	74.3	deg. F	534.3	deg. R
<b>As</b>	Area of Stack	1.97	sq ft	19.0	in. dia.
<b>Vs</b>	Stack Gas Velocity	41.67	ft/sec		
<b>Qa</b>	Actual Flow Rate	<del>4,923</del>	cfm		
<b>Qad</b>	Actual Flow Rate, Dry	4,886	dcfm		
<b>Q(std)</b>	Stack Gas Flow Rate	4,800	dscfm		
<b>An</b>	Nozzle Area	0.0002712	sq ft	0.223	in. dia.
<b>Theta</b>	Sampling Time	60	min.		
<b>I</b>	Isokinetics	95.1	%		

**FIELD DATA & CALCULATIONS SUMMARY**

Client: Hanford/Eckley  
 Site: Hanford Gln  
 Unit: Lint Trap

Date: 12/4/90  
 Type: T std = 60 F  
 Run: 1-Part

<b>Wlc</b>	Water Condensate Weight	5.5	g		
<b>Vlc</b>	Water Condensate Volume	5.5	ml		
<b>Vm</b>	Metered Sample Gas Volume	35.530	dcf		
<b>Lp</b>	Avg. Leak Rate	0.000	cf		
<b>Vn</b>	Leak Corrected Sample Gas Volume	35.530	dcf		
<b>Y</b>	Dry Gas Meter Calibration Factor	1.023			
<b>Pbar</b>	Barometric Pressure	30.10	In. Hg		
<b>Pg</b>	Static Pressure	-0.1	In. H2O		
<b>Ps</b>	Stack Pressure, Absolute	30.09	in. Hg		
<b>Δ H</b>	Dry Gas Meter Press. Differential, Average	0.979	In. H2O		
<b>Tm</b>	Dry Gas Meter Temperature, Average	81.6	deg. F	541.6	deg. R
<b>Vm(std)</b>	Sample Gas Volume	35.1947	dscf		
<b>Vm(wet)</b>	Sample Gas Volume, Wet	35.4505	scf		
<b>Vw(std)</b>	Water Vapor Volume	0.2559	scf		
<b>Bws</b>	Water Content of Stack Gas	0.007		0.7	%
<b>CO2</b>	Carbon Dioxide, Dry	0.1	%		
<b>O2</b>	Oxygen, Dry	20.9	%		
<b>N2</b>	Nitrogen, Dry	79.1	%		
<b>Md</b>	Molecular Wt. of Stack Gas, Dry	28.844	lb/lb mole		
<b>Ms</b>	Molecular Wt. of Stack Gas, Wet	28.766	lb/lb mole		
<b>Cp</b>	Pitot Calibration Factor	0.850			
<b>Δ P</b>	Velocity Head, Average Square Root	0.593	In. H2O		
<b>Ts</b>	Stack Gas Temperature, Average	105.5	deg. F	565.5	deg. R
<b>As</b>	Area of Stack	2.64	sq ft	22.0	in. dia.
<b>Vs</b>	Stack Gas Velocity	34.82	ft/sec		
<b>Qa</b>	Actual Flow Rate	5,515	cfm		
<b>Qad</b>	Actual Flow Rate, Dry	5,475	dcfm		
<b>Q(std)</b>	Stack Gas Flow Rate	5,064	dscfm		
<b>An</b>	Nozzle Area	0.0002712	sq ft	0.223	in. dia.
<b>Theta</b>	Sampling Time	7.2	min.		
<b>I</b>	Isokinetics	91.8	%		

**FIELD DATA & CALCULATIONS SUMMARY**

Client: **Hanford/Eckley**  
 Site: **Hanford Gln**  
 Unit: **Lint Trap**

Date: **12/4/90**  
 Type: **T std = 60 F**  
 Run: **2-Part**

<b>Wlc</b>	Water Condensate Weight	7.8	g		
<b>Vlc</b>	Water Condensate Volume	7.8	ml		
<b>Vm</b>	Metered Sample Gas Volume	37.737	dcf		
<b>Lp</b>	Avg. Leak Rate	0.000	cf		
<b>Vn</b>	Leak Corrected Sample Gas Volume	37.737	dcf		
<b>Y</b>	Dry Gas Meter Calibration Factor	1.023			
<b>Pbar</b>	Barometric Pressure	30.10	In. Hg		
<b>Pg</b>	Static Pressure	-0.1	In. H2O		
<b>Ps</b>	Stack Pressure, Absolute	30.09	in. Hg		
<b>Δ H</b>	Dry Gas Meter Press. Differential, Average	0.999	In. H2O		
<b>Tm</b>	Dry Gas Meter Temperature, Average	80.9	deg. F	540.9	deg. R
<b>Vm(std)</b>	Sample Gas Volume	37.4331	dscf		
<b>Vm(wet)</b>	Sample Gas Volume, Wet	37.7959	scf		
<b>Vw(std)</b>	Water Vapor Volume	0.3628	scf		
<b>Bws</b>	Water Content of Stack Gas	0.010		1.0	%
<b>CO2</b>	Carbon Dioxide, Dry	0.1	%		
<b>O2</b>	Oxygen, Dry	20.9	%		
<b>N2</b>	Nitrogen, Dry	79.1	%		
<b>Md</b>	Molecular Wt. of Stack Gas, Dry	28.844	lb/lb mole		
<b>Ms</b>	Molecular Wt. of Stack Gas, Wet	28.740	lb/lb mole		
<b>Cp</b>	Pitot Calibration Factor	0.850			
<b>Δ P</b>	Velocity Head, Average Square Root	0.598	In. H2O		
<b>Ts</b>	Stack Gas Temperature, Average	102.4	deg. F	562.4	deg. R
<b>As</b>	Area of Stack	2.64	sq ft	22.0	in. dia.
<b>Vs</b>	Stack Gas Velocity	35.03	ft/sec		
<b>Qa</b>	Actual Flow Rate	5,548	cfm		
<b>Qad</b>	Actual Flow Rate, Dry	5,495	dcfm		
<b>Q(std)</b>	Stack Gas Flow Rate	5,109	dscfm		
<b>An</b>	Nozzle Area	0.0002712	sq ft	0.223	in. dia.
<b>Theta</b>	Sampling Time	7.2	min.		
<b>I</b>	Isokinetics	96.8	%		

**FIELD DATA & CALCULATIONS SUMMARY**

Client: **Hanford/Eckley**  
 Site: **Hanford Gln**  
 Unit: **Suction**

Date: **12/3/90**  
 Type: **T std = 60 F**  
 Run: **1-Part**

<b>Wlc</b>	Water Condensate Weight	9.2	g		
<b>Vlc</b>	Water Condensate Volume	9.2	ml		
<b>Vm</b>	Metered Sample Gas Volume	44.725	dscf		
<b>Lp</b>	Avg. Leak Rate	0.000	cf		
<b>Vn</b>	Leak Corrected Sample Gas Volume	44.725	dscf		
<b>Y</b>	Dry Gas Meter Calibration Factor	0.969			
<b>Pbar</b>	Barometric Pressure	30.27	In. Hg		
<b>Pg</b>	Static Pressure	-0.03	In. H2O		
<b>Ps</b>	Stack Pressure, Absolute	30.27	in. Hg		
<b>Δ H</b>	Dry Gas Meter Press. Differential, Average	1.434	In. H2O		
<b>Tm</b>	Dry Gas Meter Temperature, Average	69.3	deg. F	529.3	deg. R
<b>Vm(std)</b>	Sample Gas Volume	43.2069	dscf		
<b>Vm(wet)</b>	Sample Gas Volume, Wet	43.6349	scf		
<b>Vw(std)</b>	Water Vapor Volume	0.4280	scf		
<b>Bws</b>	Water Content of Stack Gas	0.010		1.0	%
<b>CO2</b>	Carbon Dioxide, Dry	0.1	%		
<b>O2</b>	Oxygen, Dry	20.9	%		
<b>N2</b>	Nitrogen, Dry	79.1	%		
<b>Md</b>	Molecular Wt. of Stack Gas, Dry	28.844	lb/lb mole		
<b>Ms</b>	Molecular Wt. of Stack Gas, Wet	28.738	lb/lb mole		
<b>Cp</b>	Pitot Calibration Factor	0.850			
<b>Δ P</b>	Velocity Head, Average Square Root	0.399	In. H2O		
<b>Ts</b>	Stack Gas Temperature, Average	75.5	deg. F	535.5	deg. R
<b>As</b>	Area of Stack	2.64	sq ft	22.0	in. dia.
<b>Vs</b>	Stack Gas Velocity	22.77	ft/sec		
<b>Qa</b>	Actual Flow Rate	3,606	cfm		
<b>Qad</b>	Actual Flow Rate, Dry	3,571	dscfm		
<b>Q(std)</b>	Stack Gas Flow Rate	3,508	dscfm		
<b>An</b>	Nozzle Area	0.0004844	sq ft	0.298	in. dia.
<b>Theta</b>	Sampling Time	72	min.		
<b>I</b>	Isokinetics	96.2	%		

**FIELD DATA & CALCULATIONS SUMMARY**

Client: **Hanford/Eckley**  
 Site: **Hanford Gln**  
 Unit: **Suction**

Date: **12/3/90**  
 Type: **T std = 60 F**  
 Run: **2-Part**

<b>Wlc</b>	Water Condensate Weight	9.2	g		
<b>Vlc</b>	Water Condensate Volume	9.2	ml		
<b>Vm</b>	Metered Sample Gas Volume	37.723	dcf		
<b>Lp</b>	Avg. Leak Rate	0.000	cf		
<b>Vn</b>	Leak Corrected Sample Gas Volume	37.723	dcf		
<b>Y</b>	Dry Gas Meter Calibration Factor	0.969			
<b>Pbar</b>	Barometric Pressure	30.27	In. Hg		
<b>Pg</b>	Static Pressure	-0.03	In. H2O		
<b>Ps</b>	Stack Pressure, Absolute	30.27	in. Hg		
<b>Δ H</b>	Dry Gas Meter Press. Differential, Average	1.443	In. H2O		
<b>Tm</b>	Dry Gas Meter Temperature, Average	76.3	deg. F	536.3	deg. R
<b>Vm(std)</b>	Sample Gas Volume	35.9649	dscf		
<b>Vm(wet)</b>	Sample Gas Volume, Wet	36.3929	scf		
<b>Vw(std)</b>	Water Vapor Volume	0.4280	scf		
<b>Bws</b>	Water Content of Stack Gas	0.012		1.2	%
<b>CO2</b>	Carbon Dioxide, Dry	0.1	%		
<b>O2</b>	Oxygen, Dry	20.9	%		
<b>N2</b>	Nitrogen, Dry	79.1	%		
<b>Md</b>	Molecular Wt. of Stack Gas, Dry	28.844	lb/lb mole		
<b>Ms</b>	Molecular Wt. of Stack Gas, Wet	28.716	lb/lb mole		
<b>Cp</b>	Pitot Calibration Factor	0.850			
<b>Δ P</b>	Velocity Head, Average Square Root	0.404	In. H2O		
<b>Ts</b>	Stack Gas Temperature, Average	84.3	deg. F	544.3	deg. R
<b>As</b>	Area of Stack	2.64	sq ft	22.0	in. dia.
<b>Vs</b>	Stack Gas Velocity	23.22	ft/sec		
<b>Qa</b>	Actual Flow Rate	3,678	cfm		
<b>Qad</b>	Actual Flow Rate, Dry	3,635	dcfm		
<b>Q(std)</b>	Stack Gas Flow Rate	3,513	dscfm		
<b>An</b>	Nozzle Area	0.0004844	sq ft	0.298	in. dia.
<b>Theta</b>	Sampling Time	60	min.		
<b>I</b>	Isokinetics	96.0	%		

**FIELD DATA & CALCULATIONS SUMMARY**

Client: **Hanford/Eckley**  
 Site: **Hanford Gln**  
 Unit: **#1 Dryer**

Date: **12/3/90**  
 Type: **T std = 60 F**  
 Run: **1-Part**

<b>Wlc</b>	Water Condensate Weight	14.8	g		
<b>Vlc</b>	Water Condensate Volume	14.8	ml		
<b>Vm</b>	Metered Sample Gas Volume	44.377	dcf		
<b>Lp</b>	Avg. Leak Rate	0.000	cf		
<b>Vn</b>	Leak Corrected Sample Gas Volume	44.377	dcf		
<b>Y</b>	Dry Gas Meter Calibration Factor	0.969			
<b>Pbar</b>	Barometric Pressure	30.25	In. Hg		
<b>Pg</b>	Static Pressure	-0.06	In. H2O		
<b>Ps</b>	Stack Pressure, Absolute	30.25	in. Hg		
<b>Δ H</b>	Dry Gas Meter Press. Differential, Average	1.359	In. H2O		
<b>Tm</b>	Dry Gas Meter Temperature, Average	79.6	deg. F	539.6	deg. R
<b>Vm(std)</b>	Sample Gas Volume	42.0144	dscf		
<b>Vm(wet)</b>	Sample Gas Volume, Wet	42.7029	scf		
<b>Vw(std)</b>	Water Vapor Volume	0.6885	scf		
<b>Bws</b>	Water Content of Stack Gas	0.016		1.6	%
<b>CO2</b>	Carbon Dioxide, Dry	0.1	%		
<b>O2</b>	Oxygen, Dry	20.9	%		
<b>N2</b>	Nitrogen, Dry	79.1	%		
<b>Md</b>	Molecular Wt. of Stack Gas, Dry	28.844	lb/lb mole		
<b>Ms</b>	Molecular Wt. of Stack Gas, Wet	28.669	lb/lb mole		
<b>Cp</b>	Pitot Calibration Factor	0.850			
<b>Δ P</b>	Velocity Head, Average Square Root	0.537	In. H2O		
<b>Ts</b>	Stack Gas Temperature, Average	130.8	deg. F	590.8	deg. R
<b>As</b>	Area of Stack	1.97	sq ft	19.0	in. dia.
<b>Vs</b>	Stack Gas Velocity	32.23	ft/sec		
<b>Qa</b>	Actual Flow Rate	3,807	cfm		
<b>Qad</b>	Actual Flow Rate, Dry	3,746	dcfm		
<b>Q(std)</b>	Stack Gas Flow Rate	3,333	dscfm		
<b>An</b>	Nozzle Area	0.0003547	sq ft	0.255	in. dia.
<b>Theta</b>	Sampling Time	72	min.		
<b>I</b>	Isokinetics	100.3	%		

**FIELD DATA & CALCULATIONS SUMMARY**

Client: **Hanford/Eckley**  
 Site: **Hanford Gln**  
 Unit: **#1 Dryer**

Date: **12/3/90**  
 Type: **T std = 60 F**  
 Run: **2-Part**

<b>Wlc</b>	Water Condensate Weight	24.1	g		
<b>Vlc</b>	Water Condensate Volume	24.1	ml		
<b>Vm</b>	Metered Sample Gas Volume	42.250	dcf		
<b>Lp</b>	Avg. Leak Rate	0.000	cf		
<b>Vn</b>	Leak Corrected Sample Gas Volume	42.250	dcf		
<b>Y</b>	Dry Gas Meter Calibration Factor	0.969			
<b>Pbar</b>	Barometric Pressure	30.25	In. Hg		
<b>Pg</b>	Static Pressure	-0.06	In. H2O		
<b>Ps</b>	Stack Pressure, Absolute	30.25	in. Hg		
<b>Δ H</b>	Dry Gas Meter Press. Differential, Average	1.350	In. H2O		
<b>Tm</b>	Dry Gas Meter Temperature, Average	81.0	deg. F	541.0	deg. R
<b>Vm(std)</b>	Sample Gas Volume	39.8982	dscf		
<b>Vm(wet)</b>	Sample Gas Volume, Wet	41.0193	scf		
<b>Vw(std)</b>	Water Vapor Volume	1.1211	scf		
<b>Bws</b>	Water Content of Stack Gas	0.027		2.7	%
<b>CO2</b>	Carbon Dioxide, Dry	0.1	%		
<b>O2</b>	Oxygen, Dry	20.9	%		
<b>N2</b>	Nitrogen, Dry	79.1	%		
<b>Md</b>	Molecular Wt. of Stack Gas, Dry	28.844	lb/lb mole		
<b>Ms</b>	Molecular Wt. of Stack Gas, Wet	28.548	lb/lb mole		
<b>Cp</b>	Pitot Calibration Factor	0.850			
<b>Δ P</b>	Velocity Head, Average Square Root	0.536	In. H2O		
<b>Ts</b>	Stack Gas Temperature, Average	146.9	deg. F	606.9	deg. R
<b>As</b>	Area of Stack	1.97	sq ft	19.0	in. dia.
<b>Vs</b>	Stack Gas Velocity	32.65	ft/sec		
<b>Qa</b>	Actual Flow Rate	3,857	cfm		
<b>Qad</b>	Actual Flow Rate, Dry	3,752	dcfm		
<b>Q(std)</b>	Stack Gas Flow Rate	3,250	dscfm		
<b>An</b>	Nozzle Area	0.0003547	sq ft	0.255	in. dia.
<b>Theta</b>	Sampling Time	72	min.		
<b>I</b>	Isokinetics	97.7	%		

**FIELD DATA & CALCULATIONS SUMMARY**

Client: **Hanford/Eckley**  
 Site: **Hanford Gln**  
 Unit: **Moat**

Date: **12/4/90**  
 Type: **T std = 60 F**  
 Run: **1-PM10**

<b>Wlc</b>	Water Condensate Weight	8.0	g		
<b>Vlc</b>	Water Condensate Volume	8.0	ml		
<b>Vm</b>	Metered Sample Gas Volume	41.340	dcf		
<b>Lp</b>	Avg. Leak Rate	0.000	cf		
<b>Vn</b>	Leak Corrected Sample Gas Volume	41.340	dcf		
<b>Y</b>	Dry Gas Meter Calibration Factor	0.969			
<b>Pbar</b>	Barometric Pressure	30.21	In. Hg		
<b>Pg</b>	Static Pressure	-0.15	In. H2O		
<b>Ps</b>	Stack Pressure, Absolute	30.20	in. Hg		
<b>Δ H</b>	Dry Gas Meter Press. Differential, Average	1.253	In. H2O		
<b>Tm</b>	Dry Gas Meter Temperature, Average	62.7	deg. F	522.7	deg. R
<b>Vm(std)</b>	Sample Gas Volume	40.3391	dscf		
<b>Vm(wet)</b>	Sample Gas Volume, Wet	40.7112	scf		
<b>Vw(std)</b>	Water Vapor Volume	0.3721	scf		
<b>Bws</b>	Water Content of Stack Gas	0.009		0.9	%
<b>CO2</b>	Carbon Dioxide, Dry	0.1	%		
<b>O2</b>	Oxygen, Dry	20.9	%		
<b>N2</b>	Nitrogen, Dry	79.1	%		
<b>Md</b>	Molecular Wt. of Stack Gas, Dry	28.844	lb/lb mole		
<b>Ms</b>	Molecular Wt. of Stack Gas, Wet	28.745	lb/lb mole		
<b>Cp</b>	Pitot Calibration Factor	0.850			
<b>Δ P</b>	Velocity Head, Average Square Root	0.731	In. H2O		
<b>Ts</b>	Stack Gas Temperature, Average	61.3	deg. F	521.3	deg. R
<b>As</b>	Area of Stack	1.97	sq ft	19.0	in. dia.
<b>Vs</b>	Stack Gas Velocity	41.17	ft/sec		
<b>Qa</b>	Actual Flow Rate	4,864	cfm		
<b>Qad</b>	Actual Flow Rate, Dry	4,820	dcfm		
<b>Q(std)</b>	Stack Gas Flow Rate	4,853	dscfm		
<b>An</b>	Nozzle Area	0.0002428	sq ft	0.211	in. dia.
<b>Theta</b>	Sampling Time	72	min.		
<b>I</b>	Isokinetics	96.6	%		

**FIELD DATA & CALCULATIONS SUMMARY**

Client: **Hanford/Eckley**  
 Site: **Hanford Gln**  
 Unit: **Moat**

Date: **12/4/90**  
 Type: **T std = 60 F**  
 Run: **2-PM10**

<b>Wlc</b>	Water Condensate Weight	5.9	g		
<b>Vlc</b>	Water Condensate Volume	5.9	ml		
<b>Vm</b>	Metered Sample Gas Volume	35.231	dcf		
<b>Lp</b>	Avg. Leak Rate	0.000	cf		
<b>Vn</b>	Leak Corrected Sample Gas Volume	35.231	dcf		
<b>Y</b>	Dry Gas Meter Calibration Factor	0.969			
<b>Pbar</b>	Barometric Pressure	30.21	In. Hg		
<b>Pg</b>	Static Pressure	-0.15	In. H2O		
<b>Ps</b>	Stack Pressure, Absolute	30.20	in. Hg		
<b>Δ H</b>	Dry Gas Meter Press. Differential, Average	1.252	In. H2O		
<b>Tm</b>	Dry Gas Meter Temperature, Average	78.9	deg. F	538.9	deg. R
<b>Vm(std)</b>	Sample Gas Volume	33.3427	dscf		
<b>Vm(wet)</b>	Sample Gas Volume, Wet	33.6171	scf		
<b>Vw(std)</b>	Water Vapor Volume	0.2745	scf		
<b>Bws</b>	Water Content of Stack Gas	0.008		0.8	%
<b>CO2</b>	Carbon Dioxide, Dry	0.1	%		
<b>O2</b>	Oxygen, Dry	20.9	%		
<b>N2</b>	Nitrogen, Dry	79.1	%		
<b>Md</b>	Molecular Wt. of Stack Gas, Dry	28.844	lb/lb mole		
<b>Ms</b>	Molecular Wt. of Stack Gas, Wet	28.755	lb/lb mole		
<b>Cp</b>	Pitot Calibration Factor	0.850			
<b>Δ P</b>	Velocity Head, Average Square Root	0.729	In. H2O		
<b>Ts</b>	Stack Gas Temperature, Average	74.9	deg. F	534.9	deg. R
<b>As</b>	Area of Stack	1.97	sq ft	19.0	in. dia.
<b>Vs</b>	Stack Gas Velocity	41.59	ft/sec		
<b>Qa</b>	Actual Flow Rate	4,913	cfm		
<b>Qad</b>	Actual Flow Rate, Dry	4,873	dcfm		
<b>Q(std)</b>	Stack Gas Flow Rate	4,782	dscfm		
<b>An</b>	Nozzle Area	0.0002428	sq ft	0.211	in. dia.
<b>Theta</b>	Sampling Time	60	min.		
<b>I</b>	Isokinetics	97.3	%		

**FIELD DATA & CALCULATIONS SUMMARY**

Client: **Hanford/Eckley**  
 Site: **Hanford Gln**  
 Unit: **Lint Trap**

Date: **12/4/90**  
 Type: **T std = 60 F**  
 Run: **1-PM10**

<b>Wlc</b>	Water Condensate Weight	4.4	g		
<b>Vlc</b>	Water Condensate Volume	4.4	ml		
<b>Vm</b>	Metered Sample Gas Volume	32.419	dscf		
<b>Lp</b>	Avg. Leak Rate	0.000	cf		
<b>Vn</b>	Leak Corrected Sample Gas Volume	32.419	dscf		
<b>Y</b>	Dry Gas Meter Calibration Factor	0.969			
<b>Pbar</b>	Barometric Pressure	30.10	In. Hg		
<b>Pg</b>	Static Pressure	-0.1	In. H2O		
<b>Ps</b>	Stack Pressure, Absolute	30.09	in. Hg		
<b>Δ H</b>	Dry Gas Meter Press. Differential, Average	0.804	In. H2O		
<b>Tm</b>	Dry Gas Meter Temperature, Average	81.1	deg. F	541.1	deg. R
<b>Vm(std)</b>	Sample Gas Volume	30.4143	dscf		
<b>Vm(wet)</b>	Sample Gas Volume, Wet	30.6190	scf		
<b>Vw(std)</b>	Water Vapor Volume	0.2047	scf		
<b>Bws</b>	Water Content of Stack Gas	0.007		0.7	%
<b>CO2</b>	Carbon Dioxide, Dry	0.1	%		
<b>O2</b>	Oxygen, Dry	20.9	%		
<b>N2</b>	Nitrogen, Dry	79.1	%		
<b>Md</b>	Molecular Wt. of Stack Gas, Dry	28.844	lb/lb mole		
<b>Ms</b>	Molecular Wt. of Stack Gas, Wet	28.772	lb/lb mole		
<b>Cp</b>	Pitot Calibration Factor	0.850			
<b>Δ P</b>	Velocity Head, Average Square Root	0.598	In. H2O		
<b>Ts</b>	Stack Gas Temperature, Average	105.5	deg. F	565.5	deg. R
<b>As</b>	Area of Stack	2.64	sq ft	22.0	in. dia.
<b>Vs</b>	Stack Gas Velocity	35.14	ft/sec		
<b>Qa</b>	Actual Flow Rate	5,565	cfm		
<b>Qad</b>	Actual Flow Rate, Dry	5,528	dscfm		
<b>Q(std)</b>	Stack Gas Flow Rate	5,112	dscfm		
<b>An</b>	Nozzle Area	0.0002428	sq ft	0.211	in. dia.
<b>Theta</b>	Sampling Time	72	min.		
<b>I</b>	Isokinetics	92.7	%		

**FIELD DATA & CALCULATIONS SUMMARY**

Client: **Hanford/Eckley**  
 Site: **Hanford Gln**  
 Unit: **Lint Trap**

Date: **12/4/90**  
 Type: **T std = 60 F**  
 Run: **2-PM10**

<b>Wlc</b>	Water Condensate Weight	7.6	g		
<b>Vlc</b>	Water Condensate Volume	7.6	ml		
<b>Vm</b>	Metered Sample Gas Volume	33.678	dscf		
<b>Lp</b>	Avg. Leak Rate	0.000	cf		
<b>Vn</b>	Leak Corrected Sample Gas Volume	33.678	dscf		
<b>Y</b>	Dry Gas Meter Calibration Factor	0.969			
<b>Pbar</b>	Barometric Pressure	30.10	In. Hg		
<b>Pg</b>	Static Pressure	-0.1	In. H2O		
<b>Ps</b>	Stack Pressure, Absolute	30.09	In. Hg		
<b>Δ H</b>	Dry Gas Meter Press. Differential, Average	0.813	In. H2O		
<b>Tm</b>	Dry Gas Meter Temperature, Average	80.2	deg. F	540.2	deg. R
<b>Vm(std)</b>	Sample Gas Volume	31.6498	dscf		
<b>Vm(wet)</b>	Sample Gas Volume, Wet	32.0034	scf		
<b>Vw(std)</b>	Water Vapor Volume	0.3535	scf		
<b>Bws</b>	Water Content of Stack Gas	0.011		1.1	%
<b>CO2</b>	Carbon Dioxide, Dry	0.1	%		
<b>O2</b>	Oxygen, Dry	20.9	%		
<b>N2</b>	Nitrogen, Dry	79.1	%		
<b>Md</b>	Molecular Wt. of Stack Gas, Dry	28.844	lb/lb mole		
<b>Ms</b>	Molecular Wt. of Stack Gas, Wet	28.724	lb/lb mole		
<b>Cp</b>	Pitot Calibration Factor	0.850			
<b>Δ P</b>	Velocity Head, Average Square Root	0.602	In. H2O		
<b>Ts</b>	Stack Gas Temperature, Average	102.8	deg. F	562.8	deg. R
<b>As</b>	Area of Stack	2.64	sq ft	22.0	in. dia.
<b>Vs</b>	Stack Gas Velocity	35.30	ft/sec		
<b>Qa</b>	Actual Flow Rate	5,591	cfm		
<b>Qad</b>	Actual Flow Rate, Dry	5,529	dscfm		
<b>Q(std)</b>	Stack Gas Flow Rate	5,138	dscfm		
<b>An</b>	Nozzle Area	0.0002428	sq ft	0.211	in. dia.
<b>Theta</b>	Sampling Time	7.2	min.		
<b>I</b>	Isokinetics	96.0	%		

**FIELD DATA & CALCULATIONS SUMMARY**

Client: **Hanford/Eckley**  
 Site: **Hanford Gln**  
 Unit: **Suctlon**

Date: **12/3/90**  
 Type: **T std = 60 F**  
 Run: **1-PM10**

<b>Wlc</b>	Water Condensate Weight	8.7	g		
<b>Vlc</b>	Water Condensate Volume	8.7	ml		
<b>Vm</b>	Metered Sample Gas Volume	43.776	dcf		
<b>Lp</b>	Avg. Leak Rate	0.000	cf		
<b>Vn</b>	Leak Corrected Sample Gas Volume	43.776	dcf		
<b>Y</b>	Dry Gas Meter Calibration Factor	1.023			
<b>Pbar</b>	Barometric Pressure	30.27	in. Hg		
<b>Pg</b>	Static Pressure	-0.03	in. H2O		
<b>Ps</b>	Stack Pressure, Absolute	30.27	in. Hg		
<b>Δ H</b>	Dry Gas Meter Press. Differential, Average	1.432	in. H2O		
<b>Tm</b>	Dry Gas Meter Temperature, Average	67.6	deg. F	527.6	deg. R
<b>Vm(std)</b>	Sample Gas Volume	44.8117	dscf		
<b>Vm(wet)</b>	Sample Gas Volume, Wet	45.2164	scf		
<b>Vw(std)</b>	Water Vapor Volume	0.4047	scf		
<b>Bws</b>	Water Content of Stack Gas	0.009		0.9	%
<b>CO2</b>	Carbon Dioxide, Dry	0.1	%		
<b>O2</b>	Oxygen, Dry	20.9	%		
<b>N2</b>	Nitrogen, Dry	79.1	%		
<b>Md</b>	Molecular Wt. of Stack Gas, Dry	28.844	lb/lb mole		
<b>Ms</b>	Molecular Wt. of Stack Gas, Wet	28.747	lb/lb mole		
<b>Cp</b>	Pitot Calibration Factor	0.850			
<b>Δ P</b>	Velocity Head, Average Square Root	0.402	in. H2O		
<b>Ts</b>	Stack Gas Temperature, Average	75.5	deg. F	535.5	deg. R
<b>As</b>	Area of Stack	2.64	sq ft	22.0	in. dia.
<b>Vs</b>	Stack Gas Velocity	22.92	ft/sec		
<b>Qa</b>	Actual Flow Rate	3,631	cfm		
<b>Qad</b>	Actual Flow Rate, Dry	3,598	dcfm		
<b>Q(std)</b>	Stack Gas Flow Rate	3,535	dscfm		
<b>An</b>	Nozzle Area	0.0004779	sq ft	0.296	in. dia.
<b>Theta</b>	Sampling Time	72	min.		
<b>I</b>	Isokinetics	95.1	%		

**FIELD DATA & CALCULATIONS SUMMARY**

Client: **Hanford/Eckley**  
 Site: **Hanford Gin**  
 Unit: **Suction**

Date: **12/3/90**  
 Type: **T std = 60 F**  
 Run: **2-PM 10**

<b>Wlc</b>	Water Condensate Weight	6.8	g		
<b>Vlc</b>	Water Condensate Volume	6.8	ml		
<b>Vm</b>	Metered Sample Gas Volume	36.708	dcf		
<b>Lp</b>	Avg. Leak Rate	0.000	cf		
<b>Vn</b>	Leak Corrected Sample Gas Volume	36.708	dcf		
<b>Y</b>	Dry Gas Meter Calibration Factor	1.023			
<b>Pbar</b>	Barometric Pressure	30.27	in. Hg		
<b>Pg</b>	Static Pressure	-0.03	in. H2O		
<b>Ps</b>	Stack Pressure, Absolute	30.27	in. Hg		
<b>Δ H</b>	Dry Gas Meter Press. Differential, Average	1.424	in. H2O		
<b>Tm</b>	Dry Gas Meter Temperature, Average	71.2	deg. F	531.2	deg. R
<b>Vm(std)</b>	Sample Gas Volume	37.3222	dscf		
<b>Vm(wet)</b>	Sample Gas Volume, Wet	37.6386	scf		
<b>Vw(std)</b>	Water Vapor Volume	0.3163	scf		
<b>Bws</b>	Water Content of Stack Gas	0.008		0.8	%
<b>CO2</b>	Carbon Dioxide, Dry	0.1	%		
<b>O2</b>	Oxygen, Dry	20.9	%		
<b>N2</b>	Nitrogen, Dry	79.1	%		
<b>Md</b>	Molecular Wt. of Stack Gas, Dry	28.844	lb/lb mole		
<b>Ms</b>	Molecular Wt. of Stack Gas, Wet	28.753	lb/lb mole		
<b>Cp</b>	Pitot Calibration Factor	0.850			
<b>Δ P</b>	Velocity Head, Average Square Root	0.404	in. H2O		
<b>Ts</b>	Stack Gas Temperature, Average	84.4	deg. F	544.4	deg. R
<b>As</b>	Area of Stack	2.64	sq ft	22.0	in. dia.
<b>Vs</b>	Stack Gas Velocity	23.20	ft/sec		
<b>Qa</b>	Actual Flow Rate	3,674	cfm		
<b>Qad</b>	Actual Flow Rate, Dry	3,643	dcfm		
<b>Q(std)</b>	Stack Gas Flow Rate	3,521	dscfm		
<b>An</b>	Nozzle Area	0.0004779	sq ft	0.296	in. dia.
<b>Theta</b>	Sampling Time	60	min.		
<b>I</b>	Isokinetics	95.4	%		

**FIELD DATA & CALCULATIONS SUMMARY**

Client: **Hanford/Eckley**  
 Site: **Hanford Gln**  
 Unit: **#1 Dryer**

Date: **12/3/90**  
 Type: **T std = 60 F**  
 Run: **1-PM10**

<b>Wlc</b>	Water Condensate Weight	16.7	g		
<b>Vlc</b>	Water Condensate Volume	16.7	ml		
<b>Vm</b>	Metered Sample Gas Volume	43.153	dscf		
<b>Lp</b>	Avg. Leak Rate	0.000	cf		
<b>Vn</b>	Leak Corrected Sample Gas Volume	43.153	dscf		
<b>Y</b>	Dry Gas Meter Calibration Factor	1.023			
<b>Pbar</b>	Barometric Pressure	30.25	In. Hg		
<b>Pg</b>	Static Pressure	-0.06	In. H2O		
<b>Ps</b>	Stack Pressure, Absolute	30.25	in. Hg		
<b>Δ H</b>	Dry Gas Meter Press. Differential, Average	1.352	In. H2O		
<b>Tm</b>	Dry Gas Meter Temperature, Average	77.3	deg. F	537.3	deg. R
<b>Vm(std)</b>	Sample Gas Volume	43.3422	dscf		
<b>Vm(wet)</b>	Sample Gas Volume, Wet	44.1190	scf		
<b>Vw(std)</b>	Water Vapor Volume	0.7769	scf		
<b>Bws</b>	Water Content of Stack Gas	0.018		1.8	%
<b>CO2</b>	Carbon Dioxide, Dry	0.1	%		
<b>O2</b>	Oxygen, Dry	20.9	%		
<b>N2</b>	Nitrogen, Dry	79.1	%		
<b>Md</b>	Molecular Wt. of Stack Gas, Dry	28.844	lb/lb mole		
<b>Ms</b>	Molecular Wt. of Stack Gas, Wet	28.653	lb/lb mole		
<b>Cp</b>	Pitot Calibration Factor	0.850			
<b>Δ P</b>	Velocity Head, Average Square Root	0.536	In. H2O		
<b>Ts</b>	Stack Gas Temperature, Average	131.4	deg. F	591.4	deg. R
<b>As</b>	Area of Stack	1.97	sq ft	19.0	in. dia.
<b>Vs</b>	Stack Gas Velocity	32.20	ft/sec		
<b>Qa</b>	Actual Flow Rate	3,804	cfm		
<b>Qad</b>	Actual Flow Rate, Dry	3,737	dscfm		
<b>Q(std)</b>	Stack Gas Flow Rate	3,321	dscfm		
<b>An</b>	Nozzle Area	0.0003773	sq ft	0.263	in. dia.
<b>Theta</b>	Sampling Time	72	min.		
<b>I</b>	Isokinetics	92.5	%		

**FIELD DATA & CALCULATIONS SUMMARY**

Client: Hanford/Eckley  
 Site: Hanford Gln  
 Unit: #1 Dryer

Date: 12/3/90  
 Type: T std = 60 F  
 Run: 2-PM10

<b>Wlc</b>	Water Condensate Weight	20.6	g		
<b>Vlc</b>	Water Condensate Volume	20.6	ml		
<b>Vm</b>	Metered Sample Gas Volume	42.760	dcf		
<b>Lp</b>	Avg. Leak Rate	0.000	cf		
<b>Vn</b>	Leak Corrected Sample Gas Volume	42.760	dcf		
<b>Y</b>	Dry Gas Meter Calibration Factor	1.023			
<b>Pbar</b>	Barometric Pressure	30.25	In. Hg		
<b>Pg</b>	Static Pressure	-0.06	In. H2O		
<b>Ps</b>	Stack Pressure, Absolute	30.25	in. Hg		
<b>Δ H</b>	Dry Gas Meter Press. Differential, Average	1.340	In. H2O		
<b>Tm</b>	Dry Gas Meter Temperature, Average	78.7	deg. F	538.7	deg. R
<b>Vm(std)</b>	Sample Gas Volume	42.8350	dscf		
<b>Vm(wet)</b>	Sample Gas Volume, Wet	43.7932	scf		
<b>Vw(std)</b>	Water Vapor Volume	0.9583	scf		
<b>Bws</b>	Water Content of Stack Gas	0.022		2.2	%
<b>CO2</b>	Carbon Dioxide, Dry	0.1	%		
<b>O2</b>	Oxygen, Dry	20.9	%		
<b>N2</b>	Nitrogen, Dry	79.1	%		
<b>Md</b>	Molecular Wt. of Stack Gas, Dry	28.844	lb/lb mole		
<b>Ms</b>	Molecular Wt. of Stack Gas, Wet	28.607	lb/lb mole		
<b>Cp</b>	Pitot Calibration Factor	0.850			
<b>Δ P</b>	Velocity Head, Average Square Root	0.536	In. H2O		
<b>Ts</b>	Stack Gas Temperature, Average	147.2	deg. F	607.2	deg. R
<b>As</b>	Area of Stack	1.97	sq ft	19.0	in. dia.
<b>Vs</b>	Stack Gas Velocity	32.65	ft/sec		
<b>Qa</b>	Actual Flow Rate	3,857	cfm		
<b>Qad</b>	Actual Flow Rate, Dry	3,773	dcfm		
<b>Q(std)</b>	Stack Gas Flow Rate	3,266	dscfm		
<b>An</b>	Nozzle Area	0.0003773	sq ft	0.263	in. dia.
<b>Theta</b>	Sampling Time	72	min.		
<b>I</b>	Isokinetics	93.0	%		

### **III. WET TEST METHODS CALCULATIONS**

**CALCULATED EMISSION RESULTS**

Client: Hanford/Eckley

Site: Hanford Gin

Unit: Moat

Date: 12/4/90

Type: T std = 60 F

Run: 1-Part

**Total Particulate**

<b>Ws</b>	Total Particulate Weight	0.1396	g
<b>Cs</b>	Total Particulate Emissions	0.0458	grain/dscf
<b>CFs</b>	Particulate Flow Rate	1.91	lb/hr

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**CALCULATED EMISSION RESULTS**

Client: **Hanford/Eckley**  
Site: **Hanford Gln**  
Unit: **Moat**

Date: **12/4/90**  
Type: **T std = 60 F**  
Run: **2-Part**

**Total Particulate**

<b>Ws</b>	Total Particulate Weight	0.4136	g
<b>Cs</b>	Total Particulate Emissions	0.1653	grain/dscf
<b>CFs</b>	Particulate Flow Rate	6.80	lb/hr

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**CALCULATED EMISSION RESULTS**

Client: **Hanford/Eckley**  
Site: **Hanford Gln**  
Unit: **Lint Trap**

Date: **12/4/90**  
Type: **T std = 60 F**  
Run: **1-Part**

**Total Particulate**

<b>Ws</b>	Total Particulate Weight	0.1218	g
<b>Cs</b>	Total Particulate Emissions	0.0534	grain/dscf
<b>CFs</b>	Particulate Flow Rate	2.32	lb/hr

*BTC Environmental, Inc. - 1989*

**CALCULATED EMISSION RESULTS**

Client: Hanford/Eckley

Site: Hanford Gln

Unit: Lint Trap

Date: 12/4/90

Type: T std = 60 F

Run: 2-Part

**Total Particulate**

<b>Ws</b>	Total Particulate Weight	0.1618	g
<b>Cs</b>	Total Particulate Emissions	0.0667	grain/dscf
<b>CFs</b>	Particulate Flow Rate	2.92	lb/hr

*BTC Environmental, Inc. - 1989*

**CALCULATED EMISSION RESULTS**

Client: Hanford/Eckley  
Site: Hanford Gln  
Unit: Suction

Date: 12/3/90  
Type: T std = 60 F  
Run: 1-Part

**Total Particulate**

<b>Ws</b>	Total Particulate Weight	0.1073	g
<b>Cs</b>	Total Particulate Emissions	0.0383	grain/dscf
<b>CFs</b>	Particulate Flow Rate	1.15	lb/hr

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**CALCULATED EMISSION RESULTS**

Client: Hanford/Eckley  
Site: Hanford Gln  
Unit: Suction

Date: 12/3/90  
Type: T std = 60 F  
Run: 2-Part

**Total Particulate**

<b>Ws</b>	Total Particulate Weight	0.0973	g
<b>Cs</b>	Total Particulate Emissions	0.0417	grain/dscf
<b>CFs</b>	Particulate Flow Rate	1.26	lb/hr

*BTC Environmental, Inc. - 1989*

**CALCULATED EMISSION RESULTS**

Client: Hanford/Eckley  
Site: Hanford Gln  
Unit: #1 Dryer

Date: 12/3/90  
Type: T std = 60 F  
Run: 1-Part

**Total Particulate**

<b>Ws</b>	Total Particulate Weight	0.0933	g
<b>Cs</b>	Total Particulate Emissions	0.0343	grain/dscf
<b>CFs</b>	Particulate Flow Rate	0.98	lb/hr

*BTC Environmental, Inc. - 1989*

**CALCULATED EMISSION RESULTS**

Client: Hanford/Eckley  
Site: Hanford Gln  
Unit: #1 Dryer

Date: 12/3/90  
Type: T std = 60 F  
Run: 2-Part

**Total Particulate**

<b>Ws</b>	Total Particulate Weight	0.2195	g
<b>Cs</b>	Total Particulate Emissions	0.0849	grain/dscf
<b>CFs</b>	Particulate Flow Rate	2.36	lb/hr

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**PARTICULATE WEIGHTS : DATA & CALCULATIONS**

Client : <u>Hanford/Eckley</u>	Date : <u>12/4/90</u>
Site : <u>Hanford Gin</u>	Job # : <u>5019</u>
Unit : <u>Moat</u>	Lab # : <u>290-188</u>
Run : <u>1</u>	

**BLANKS**

Acetone		Volume: <u>100</u> ml
Gross: <u>73.2865</u> gms.	Tare: <u>73.2842</u> gms.	Residue: <u>0.0023</u> gms.
DI Water		Volume: <u>100</u> ml
Gross: <u>71.7775</u> gms.	Tare: <u>71.7764</u> gms.	Residue: <u>0.0011</u> gms.

**WEIGHTS & VOLUMES**

Filter	Gross: <u>0.1008</u> gms.	Tare: <u>0.0891</u> gms.	Net: <u>0.0117</u> gms.
Filter	Gross: <u>0.1021</u> gms.	Tare: <u>0.0885</u> gms.	Net: <u>0.0136</u> gms.

+10 μ Rinse -			
Acetone: <u>100</u> ml *	<u>2E-05</u> gms./ml	=	Net: <u>-0.0023</u> gms.
DI Water: <u>100</u> ml *	<u>1E-05</u> gms./ml	=	Net: <u>-0.0011</u> gms.
Gross: <u>68.2542</u> gms.	Tare: <u>68.0022</u> gms.		Net: <u>0.2520</u> gms.

+10μ Total Weight = 0.2739 gms.

Filter	Gross: <u>0.2124</u> gms.	Tare: <u>0.1204</u> gms.	Net: <u>0.0920</u> gms.
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-10 μ Rinse			
DI Water: <u>400</u> ml *	<u>1E-05</u> gms./ml	=	Net: <u>-0.0044</u> gms.
Acetone: <u>50</u> ml *	<u>2E-05</u> gms./ml	=	Net: <u>-0.0012</u> gms.
Total: <u>400</u> ml	Aliquot: <u>400</u> ml		
Gross: <u>70.7180</u> gms.	Tare: <u>70.7108</u> gms.		Net: <u>0.0016</u> gms.

-10μ Total Weight = 0.0881 gms.

Total Weight = 0.3620 gms.

+ 10 μ	<u>0.7566</u> %
- 10 μ	<u>0.2434</u> %



**PARTICULATE WEIGHTS : DATA & CALCULATIONS**

Client : Hanford/Eckley Date : 12/4/90  
Site : Hanford Gin Job # : 5019  
Unit : Lint Trap Lab # : 290-188  
Run : 1

**BLANKS**

Acetone Volume: 100 ml  
Gross: 73.2865 gms. Tare: 73.2842 gms. Residue: 0.0023 gms.  
DI Water Volume: 100 ml  
Gross: 71.7775 gms. Tare: 71.7764 gms. Residue: 0.0011 gms.

**WEIGHTS & VOLUMES**

Filter Gross: 0.0916 gms. Tare: 0.0885 gms. Net: 0.0031 gms.  
Filter Gross: 0.0912 gms. Tare: 0.0591 gms. Net: 0.0321 gms.

+10  $\mu$  Rinse -  
Acetone: 100 ml \* 2E-05 gms./ml = Net: -0.0023 gms.  
DI Water: 100 ml \* 1E-05 gms./ml = Net: -0.0011 gms.  
Gross: 69.0416 gms. Tare: 68.9736 gms. Net: 0.0680 gms.

+10 $\mu$  Total Weight = 0.0998 gms.

Filter Gross: 0.1783 gms. Tare: 0.1187 gms. Net: 0.0596 gms.

-10  $\mu$  Rinse  
DI Water: 400 ml \* 1E-05 gms./ml = Net: -0.0044 gms.  
Acetone: 50 ml \* 2E-05 gms./ml = Net: -0.0012 gms.  
Total: 400 ml Aliquot: 400 ml  
Gross: 65.1148 gms. Tare: 65.1088 gms. Net: 0.0004 gms.

-10 $\mu$  Total Weight = 0.0545 gms.

Total Weight = 0.1543 gms.

+ 10  $\mu$  0.6468 %  
- 10  $\mu$  0.3532 %

**PARTICULATE WEIGHTS : DATA & CALCULATIONS**

Client : <u>Hanford/Eckley</u>	Date : <u>12/4/90</u>
Site : <u>Hanford Gin</u>	Job # : <u>5019</u>
Unit : <u>Lint Trap</u>	Lab # : <u>290-188</u>
Run : <u>2</u>	

**BLANKS**

Acetone	Gross: <u>73.2865</u> gms.	Tare: <u>73.2842</u> gms.	Volume: <u>100</u> ml	Residue: <u>0.0023</u> gms.
DI Water	Gross: <u>71.7775</u> gms.	Tare: <u>71.7764</u> gms.	Volume: <u>100</u> ml	Residue: <u>0.0011</u> gms.

**WEIGHTS & VOLUMES**

Filter	Gross: <u>0.0924</u> gms.	Tare: <u>0.0889</u> gms.	Net: <u>0.0035</u> gms.
Filter	Gross: <u>0.0928</u> gms.	Tare: <u>0.0893</u> gms.	Net: <u>0.0035</u> gms.

+10 μ Rinse -			
Acetone:	<u>100</u> ml *	<u>2E-05</u> gms./ml	= Net: <u>-0.0023</u> gms.
DI Water:	<u>100</u> ml *	<u>1E-05</u> gms./ml	= Net: <u>-0.0011</u> gms.
Gross:	<u>68.3186</u> gms.	Tare: <u>68.2537</u> gms.	Net: <u>0.0649</u> gms.

+10μ Total Weight = 0.0685 gms.

Filter	Gross: <u>0.1795</u> gms.	Tare: <u>0.1194</u> gms.	Net: <u>0.0601</u> gms.
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-10 μ Rinse			
DI Water:	<u>400</u> ml *	<u>1E-05</u> gms./ml	= Net: <u>-0.0044</u> gms.
Acetone:	<u>50</u> ml *	<u>2E-05</u> gms./ml	= Net: <u>-0.0012</u> gms.
Total:	<u>400</u> ml	Aliquot: <u>400</u> ml	
Gross:	<u>72.4737</u> gms.	Tare: <u>72.4650</u> gms.	Net: <u>0.0031</u> gms.

-10μ Total Weight = 0.0577 gms.

Total Weight = 0.1262 gms.

+ 10 μ	<u>0.5428</u> %
- 10 μ	<u>0.4572</u> %

**PARTICULATE WEIGHTS : DATA & CALCULATIONS**

Client : <u>Hanford/Eckley</u>	Date : <u>12/3/90</u>
Site : <u>Hanford Gin</u>	Job # : <u>5019</u>
Unit : <u>Suction</u>	Lab # : <u>290-188</u>
Run : <u>1</u>	

**BLANKS**

Acetone	Gross: <u>73.2865</u> gms.	Tare: <u>73.2842</u> gms.	Volume: <u>100</u> ml	Residue: <u>0.0023</u> gms.
DI Water	Gross: <u>71.7775</u> gms.	Tare: <u>71.7764</u> gms.	Volume: <u>100</u> ml	Residue: <u>0.0011</u> gms.

**WEIGHTS & VOLUMES**

Filter	Gross: <u>0.0917</u> gms.	Tare: <u>0.0901</u> gms.	Net: <u>0.0016</u> gms.
Filter	Gross: <u>0.0889</u> gms.	Tare: <u>0.0871</u> gms.	Net: <u>0.0018</u> gms.
+10 μ Rinse -			
Acetone:	<u>100</u> ml * <u>2E-05</u> gms./ml	=	Net: <u>-0.0023</u> gms.
DI Water:	<u>100</u> ml * <u>1E-05</u> gms./ml	=	Net: <u>-0.0011</u> gms.
Gross:	<u>73.9158</u> gms.	Tare: <u>73.9156</u> gms.	Net: <u>0.0002</u> gms.
	<b>+10μ Total Weight</b>	=	<u>0.0002</u> gms.
Filter	Gross: <u>0.1589</u> gms.	Tare: <u>0.1134</u> gms.	Net: <u>0.0455</u> gms.
-10 μ Rinse			
DI Water:	<u>400</u> ml * <u>1E-05</u> gms./ml	=	Net: <u>-0.0044</u> gms.
Acetone:	<u>50</u> ml * <u>2E-05</u> gms./ml	=	Net: <u>-0.0012</u> gms.
Total:	<u>400</u> ml	Aliquot: <u>400</u> ml	
Gross:	<u>73.9456</u> gms.	Tare: <u>73.9098</u> gms.	Net: <u>0.0302</u> gms.
	<b>-10μ Total Weight</b>	=	<u>0.0702</u> gms.
	<b>Total Weight</b>	=	<u>0.0704</u> gms.
	+ 10 μ		<u>0.0028</u> %
	- 10 μ		<u>0.9972</u> %

**PARTICULATE WEIGHTS : DATA & CALCULATIONS**

Client : <u>Hanford/Eckley</u>	Date : <u>12/3/90</u>
Site : <u>Hanford Gin</u>	Job # : <u>5019</u>
Unit : <u>Suction</u>	Lab # : <u>290-188</u>
Run : <u>2</u>	

**BLANKS**

Acetone	Gross: <u>73.2865</u> gms.	Tare: <u>73.2842</u> gms.	Volume: <u>100</u> ml	Residue: <u>0.0023</u> gms.
DI Water	Gross: <u>71.7775</u> gms.	Tare: <u>71.7764</u> gms.	Volume: <u>100</u> ml	Residue: <u>0.0011</u> gms.

**WEIGHTS & VOLUMES**

Filter	Gross: <u>0.0888</u> gms.	Tare: <u>0.0875</u> gms.	Net: <u>0.0013</u> gms.
Filter	Gross: <u>0.0902</u> gms.	Tare: <u>0.0891</u> gms.	Net: <u>0.0011</u> gms.

+10 μ Rinse -

Acetone:	<u>100</u> ml * <u>2E-05</u> gms./ml	=	Net: <u>-0.0023</u> gms.
DI Water:	<u>100</u> ml * <u>1E-05</u> gms./ml	=	Net: <u>-0.0011</u> gms.
Gross:	<u>73.9168</u> gms.	Tare: <u>73.9156</u> gms.	Net: <u>0.0012</u> gms.

**+10μ Total Weight = 0.0002 gms.**

Filter	Gross: <u>0.1509</u> gms.	Tare: <u>0.1173</u> gms.	Net: <u>0.0336</u> gms.
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-10 μ Rinse

DI Water:	<u>400</u> ml * <u>1E-05</u> gms./ml	=	Net: <u>-0.0044</u> gms.
Acetone :	<u>50</u> ml * <u>2E-05</u> gms./ml	=	Net: <u>-0.0012</u> gms.
Total:	<u>400</u> ml	Aliquot: <u>400</u> ml	
Gross:	<u>72.4668</u> gms.	Tare: <u>72.4602</u> gms.	Net: <u>0.0010</u> gms.

**-10μ Total Weight = 0.0291 gms.**

**Total Weight = 0.0293 gms.**

+ 10 μ	<u>0.0068</u> %
- 10 μ	<u>0.9932</u> %

**PARTICULATE WEIGHTS : DATA & CALCULATIONS**

Client : <u>Hanford/Eckley</u>	Date : <u>12/3/90</u>
Site : <u>Hanford Gin</u>	Job # : <u>5019</u>
Unit : <u>Drier</u>	Lab # : <u>290-188</u>
Run : <u>1</u>	

**BLANKS**

Acetone		Volume: <u>100</u> ml
Gross: <u>73.2865</u> gms.	Tare: <u>73.2842</u> gms.	Residue: <u>0.0023</u> gms.
DI Water		Volume: <u>100</u> ml
Gross: <u>71.7775</u> gms.	Tare: <u>71.7764</u> gms.	Residue: <u>0.0011</u> gms.

**WEIGHTS & VOLUMES**

Filter	Gross: <u>0.0903</u> gms.	Tare: <u>0.0883</u> gms.	Net: <u>0.0020</u> gms.
Filter	Gross: <u>0.0912</u> gms.	Tare: <u>0.0889</u> gms.	Net: <u>0.0023</u> gms.

+10 μ Rinse -			
Acetone:	<u>100</u> ml * <u>2E-05</u> gms./ml	=	Net: <u>-0.0023</u> gms.
DI Water:	<u>100</u> ml * <u>1E-05</u> gms./ml	=	Net: <u>-0.0011</u> gms.
Gross:	<u>68.0188</u> gms.	Tare: <u>67.9752</u> gms.	Net: <u>0.0436</u> gms.

+10μ Total Weight = 0.0445 gms.

Filter	Gross: <u>0.1554</u> gms.	Tare: <u>0.1182</u> gms.	Net: <u>0.0372</u> gms.
--------	---------------------------	--------------------------	-------------------------

-10 μ Rinse			
DI Water:	<u>400</u> ml * <u>1E-05</u> gms./ml	=	Net: <u>-0.0044</u> gms.
Acetone:	<u>50</u> ml * <u>2E-05</u> gms./ml	=	Net: <u>-0.0012</u> gms.
Total:	<u>400</u> ml	Aliquot: <u>400</u> ml	
Gross:	<u>69.2162</u> gms.	Tare: <u>69.2099</u> gms.	Net: <u>0.0007</u> gms.

-10μ Total Weight = 0.0323 gms.

Total Weight = 0.0768 gms.

+ 10 μ	<u>0.5791</u> %
- 10 μ	<u>0.4209</u> %

**PARTICULATE WEIGHTS : DATA & CALCULATIONS**

Client : <u>Hanford/Eckley</u>	Date : <u>12/3/90</u>
Site : <u>Hanford Gin</u>	Job # : <u>5019</u>
Unit : <u>Drier</u>	Lab # : <u>290-188</u>
Run : <u>2</u>	

**BLANKS**

Acetone		Volume: <u>100</u> ml
Gross: <u>73.2865</u> gms.	Tare: <u>73.2842</u> gms.	Residue: <u>0.0023</u> gms.
DI Water		Volume: <u>100</u> ml
Gross: <u>71.7775</u> gms.	Tare: <u>71.7764</u> gms.	Residue: <u>0.0011</u> gms.

**WEIGHTS & VOLUMES**

Filter	Gross: <u>0.0941</u> gms.	Tare: <u>0.0891</u> gms.	Net: <u>0.0050</u> gms.
Filter	Gross: <u>0.0960</u> gms.	Tare: <u>0.0891</u> gms.	Net: <u>0.0069</u> gms.
+10 μ Rinse -			
Acetone:	<u>100</u> ml * <u>2E-05</u> gms./ml	=	Net: <u>-0.0023</u> gms.
DI Water:	<u>100</u> ml * <u>1E-05</u> gms./ml	=	Net: <u>-0.0011</u> gms.
Gross:	<u>69.2174</u> gms.	Tare: <u>69.1140</u> gms.	Net: <u>0.1034</u> gms.
	<b>+10μ Total Weight</b>	=	<u>0.1119</u> gms.
Filter	Gross: <u>0.1851</u> gms.	Tare: <u>0.1166</u> gms.	Net: <u>0.0685</u> gms.
-10 μ Rinse			
DI Water:	<u>400</u> ml * <u>1E-05</u> gms./ml	=	Net: <u>-0.0044</u> gms.
Acetone:	<u>50</u> ml * <u>2E-05</u> gms./ml	=	Net: <u>-0.0012</u> gms.
Total:	<u>400</u> ml	Aliquot: <u>400</u> ml	
Gross:	<u>70.8788</u> gms.	Tare: <u>70.8696</u> gms.	Net: <u>0.0036</u> gms.
	<b>-10μ Total Weight</b>	=	<u>0.0666</u> gms.
	<b>Total Weight</b>	=	<u>0.1785</u> gms.
	+ 10 μ		<u>0.6269</u> %
	- 10 μ		<u>0.3731</u> %

## **V. LABORATORY ANALYSIS**

**Run Set Up Sheet**

Client : Hanford/Eckley  
 Site : Hanford Gin  
 Unit: Moat

Date : 12/4/90  
 Job #: 5019  
 Lab #: 290-188

Method#: 5  
 Run#: 1  
 Hot box#: -

Probe#: 7  
 Stack box#: E  
 Cold box#: 5

Pryo#: T-5  
 Nozzle#: 0.223  
 Pitot#: 0.85

Imp. #1: 

gross	598.9
tare	598.8
final	<u>0.1</u>

Imp. #2: 

gross	603.5
tare	604.0
final	<u>-0.5</u>

Imp. #3: 

gross	466.9
tare	466.4
final	<u>0.5</u>

Imp. #4: 

gross	607.3
tare	598.3
final	<u>9.0</u>

Total 9.1

Probe blank 

-
---

 ml  
 Probe rinse 

200
-----

 ml

Solution blank 

DI
----

  
 Solution blank 

Acetone
---------

Filter No: 

D-24
------

  
 Filter Tare wt. 

--

	#	date
Solution Container		
Solution Container		

Sample Vol: 

start	150.0	
Imp#1	finsh	150.1

 ml  
 Amount Gained: 0.1 ml

Sample Vol: 

start	150.0	
Imp #2	finsh	149.5

 ml  
 Amount Gained: -0.5 ml

Total Vol #1 #2 & Rinse 400.0 ml

Comments: \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_

**Run Set Up Sheet**

Client : Hanford/Eckley  
 Site : Hanford Gin  
 Unit: Moat

Date : 12/4/90  
 Job #: 5019  
 Lab #: 290-188

Method#: 5  
 Run#: 2  
 Hot box#: -

Probe#: 7  
 Stack box#: E  
 Cold box#: 10

Pryo#: T-5  
 Nozzle#: 0.223  
 Pitot#: 0.85

Imp. #1: 

gross	588.5
tare	589.5
final	<u>-1.0</u>

Imp. #2: 

gross	600.4
tare	600.0
final	<u>0.4</u>

Imp. #3: 

gross	469.4
tare	469.9
final	<u>-0.5</u>

Imp. #4: 

gross	623.0
tare	615.7
final	<u>7.3</u>

Total 6.2

Probe blank 

-	ml
---	----

  
 Probe rinse 

200	ml
-----	----

Solution blank 

DI
----

  
 Solution blank 

Acetone
---------

Filter No: 

D-25
------

  
 Filter Tare wt. 

--

	#	date
Solution Container		
Solution Container		

Sample Vol: 

start	150.0	ml	
Imp #1	finsh	149.0	ml

  
 Amount Gained: -1.0 ml

Sample Vol: 

start	150.0	ml	
Imp #2	finsh	150.4	ml

  
 Amount Gained: 0.4 ml

Total Vol #1 #2 & Rinse 400.0 ml

Comments: \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_

**Run Set Up Sheet**

Client : Hanford/Eckley  
 Site : Hanford Gin  
 Unit: Lint Trap

Date : 12/4/90  
 Job #: 5019  
 Lab #: 290-188

Method#: 5  
 Run#: 1  
 Hot box#: -

Probe#: 7  
 Stack box#: E  
 Cold box#: 5

Pryo#: T-5  
 Nozzle#: 0.223  
 Pitot#: 0.85

Imp. #1: 

gross	591.3
tare	593.0
final	<u>-1.7</u>

Imp. #2: 

gross	624.3
tare	624.6
final	<u>-0.3</u>

Imp. #3: 

gross	466.7
tare	466.6
final	<u>0.1</u>

Imp. #4: 

gross	614.4
tare	607.0
final	<u>7.4</u>

Total 5.5

Probe blank 

-	ml
---	----

  
 Probe rinse 

200	ml
-----	----

Solution blank 

DI
----

  
 Solution blank 

Acetone
---------

Filter No: 

D-26
------

  
 Filter Tare wt. 

--

	#	date
Solution Container		
Solution Container		

Sample Vol: 

start	150.0	ml	
Imp#1	finsh	148.3	ml

  
 Amount Gained: -1.7 ml

Sample Vol: 

start	150.0	ml	
Imp #2	finsh	149.7	ml

  
 Amount Gained: -0.3 ml

Total Vol #1 #2 & Rinse 400.0 ml

Comments: \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_

**Run Set Up Sheet**

Client : Hanford/Eckley  
 Site : Hanford Gin  
 Unit: Lint Trap

Date : 12/4/90  
 Job #: 5019  
 Lab #: 290-188

Method#: 5  
 Run#: 2  
 Hot box#: -

Probe#: 7  
 Stack box#: E  
 Cold box#: 10

Pryo#: T-5  
 Nozzle#: 0.223  
 Pitot#: 0.85

Imp. #1: 

gross	600.5
tare	602.4
final	-1.9

Imp. #2: 

gross	593.5
tare	593.4
final	0.1

Imp. #3: 

gross	469.0
tare	469.3
final	-0.3

Imp. #4: 

gross	632.9
tare	623.0
final	9.9

Total 7.8

Probe blank 

-	ml
---	----

  
 Probe rinse 

200	ml
-----	----

Solution blank 

DI
----

  
 Solution blank 

Acetone
---------

Filter No: 

D-27
------

  
 Filter Tare wt. 

--

	#	date
Solution Container		
Solution Container		

Sample Vol: 

start	150.0	ml	
Imp #1	finsh	148.1	ml

  
 Amount Gained: -1.9 ml

Sample Vol: 

start	150.0	ml	
Imp #2	finsh	150.1	ml

  
 Amount Gained: 0.1 ml

Total Vol #1 #2 & Rinse 400.0 ml

Comments: \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_

**Run Set Up Sheet**

Client : Hanford/Eckley  
 Site : Hanford Gin  
 Unit: Suction

Date : 12/3/90  
 Job #: 5019  
 Lab #: 290-188

Method#: 5  
 Run#: 1  
 Hot box#: -

Probe#: 7  
 Stack box#: D  
 Cold box#: 5

Pryo#: T-5  
 Nozzle#: 0.298  
 Pitot#: 0.85

Imp. #1: 

gross	583.5
tare	583.3
final	<u>0.2</u>

Imp. #2: 

gross	604.9
tare	605.1
final	<u>-0.2</u>

Imp. #3: 

gross	465.7
tare	465.0
final	<u>0.7</u>

Imp. #4: 

gross	607.3
tare	598.8
final	<u>8.5</u>

Total 9.2

Probe blank 

-	ml
---	----

  
 Probe rinse 

200	ml
-----	----

Solution blank 

DI
----

  
 Solution blank 

Acetone
---------

Filter No: 

D-20
------

  
 Filter Tare wt. 

--

	#	date
Solution Container		
Solution Container		

Sample Vol: 

start	150.0	ml	
Imp #1	finsh	150.2	ml

  
 Amount Gained: 5.1 ml

Sample Vol: 

start	150.0	ml	
Imp #2	finsh	149.8	ml

  
 Amount Gained: -0.2 ml

Total Vol #1 #2 & Rinse 400.0 ml

Comments: \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_

**Run Set Up Sheet**

Client : Hanford/Eckley  
 Site : Hanford Gin  
 Unit: Suction

Date : 12/3/90  
 Job #: 5019  
 Lab #: 290-188

Method#: 5  
 Run#: 2  
 Hot box#: -

Probe#: 7  
 Stack box#: D  
 Cold box#: 10

Pryo#: T-5  
 Nozzle#: 0.298  
 Pitot#: 0.85

Imp. #1: 

gross	604.9
tare	605.3
final	<u>-0.4</u>

Imp. #2: 

gross	582.1
tare	580.5
final	<u>1.6</u>

Imp. #3: 

gross	469.0
tare	468.4
final	<u>0.6</u>

Imp. #4: 

gross	620.8
tare	613.4
final	<u>7.4</u>

Total 9.2

Probe blank - ml  
 Probe rinse 200 ml

Solution blank DI  
 Solution blank Acetone

Filter No: D-21  
 Filter Tare wt.

	#	date
Solution Container		
Solution Container		

Sample Vol: 

start	150.0	ml
Imp#1	finsh	149.6

  
 Amount Gained: -0.4 ml

Sample Vol: 

start	150.0	ml
Imp #2	finsh	151.6

  
 Amount Gained: 1.6 ml

Total Vol #1 #2 & Rinse 400.0 ml

Comments: \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_

### Run Set Up Sheet

Client : Hanford/Eckley  
 Site : Hanford Gin  
 Unit: #1 Dryer

Date : 12/3/90  
 Job #: 5019  
 Lab #: 290-188

Method#: 5  
 Run#: 1  
 Hot box#: -

Probe#: 7  
 Stack box#: D  
 Cold box#: 5

Pryo#: T-5  
 Nozzle#: 0.255  
 Pitot#: 0.85

Imp. #1: 

gross	604.4
tare	597.8
final	6.6

Imp. #2: 

gross	606.6
tare	604.6
final	2.0

Imp. #3: 

gross	466.5
tare	465.7
final	0.8

Imp. #4: 

gross	612.7
tare	607.3
final	5.4

Total 14.8

Probe blank 

-
---

 ml  
 Probe rinse 

200
-----

 ml

Solution blank 

DI
----

  
 Solution blank 

Acetone
---------

Filter No: 

D-22
------

  
 Filter Tare wt. 

--

	#	date
Solution Container		
Solution Container		

Sample Vol: 

start	150.0	ml	
Imp#1	finsh	156.6	ml

  
 Amount Gained: 6.6 ml

Sample Vol: 

start	150.0	ml	
Imp #2	finsh	152.0	ml

  
 Amount Gained: 2.0 ml

Total Vol #1 #2 & Rinse 400.0 ml

Comments: \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_

**Run Set Up Sheet**

Client : Hanford/Eckley  
 Site : Hanford Gin  
 Unit: #1 Dryer

Date : 12/3/90  
 Job #: 5019  
 Lab #: 290-188

Method#: 5  
 Run#: 2  
 Hot box#: -

Probe#: 7  
 Stack box#: D  
 Cold box#: 10

Pryo#: T-5  
 Nozzle#: 0.255  
 Pitot#: 0.85

Imp. #1: 

gross	604.3
tare	595.1
final	<u>9.2</u>

Imp. #2: 

gross	617.8
tare	614.7
final	<u>3.1</u>

Imp. #3: 

gross	470.0
tare	469.0
final	<u>1.0</u>

Imp. #4: 

gross	631.4
tare	620.6
final	<u>10.8</u>

Total 24.1

Probe blank - ml  
 Probe rinse 200 ml

Solution blank DI  
 Solution blank Acetone

Filter No: D-23  
 Filter Tare wt.           

	#	date
Solution Container		
Solution Container		

Sample Vol: 

start	150.0	ml	
Imp#1	finsh	159.2	ml

  
 Amount Gained: 9.2 ml

Sample Vol: 

start	150.0	ml	
Imp #2	finsh	153.1	ml

  
 Amount Gained: 3.1 ml

Total Vol #1 #2 & Rinse 400.0 ml

Comments: \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_

**Run Set Up Sheet**

Client : Hanford/Eckley  
 Site : Hanford Gin  
 Unit: Moat

Date : 12/4/90  
 Job #: 5019  
 Lab #: 290-188

Method#: PM-10  
 Run#: 1  
 Hot box#: -

Probe#: 7  
 Stack box#: D  
 Cold box#: 4

Pryo#: T-5  
 Nozzle#: 0.211  
 Pitot#: 0.85

Imp. #1: 

gross	594.0
tare	594.0
final	0.0

Imp. #2: 

gross	621.4
tare	621.3
final	0.1

Imp. #3: 

gross	476.6
tare	476.4
final	0.2

Imp. #4: 

gross	629.5
tare	621.8
final	7.7

Total 8.0

Probe blank - ml  
 Probe rinse 200 ml

Solution blank DI  
 Solution blank Acetone

Filter No: F4,X41,X42  
 Filter Tare wt.         

	#	date
Solution Container		
Solution Container		

Sample Vol: 

start	150.0	ml	
Imp #1	finsh	150.0	ml

  
 Amount Gained: 0.0 ml

Sample Vol: 

start	150.0	ml	
Imp #2	finsh	150.1	ml

  
 Amount Gained: 0.1 ml

Total Vol #1 #2 & Rinse 400.0 ml

Comments: \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_

**Run Set Up Sheet**

Client : Hanford/Eckley  
 Site : Hanford Gin  
 Unit: Moat

Date : 12/4/90  
 Job #: 5019  
 Lab #: 290-188

Method#: PM-10  
 Run#: 2  
 Hot box#: -

Probe#: 7  
 Stack box#: D  
 Cold box#: 9

Pryo#: T-5  
 Nozzle#: 0.211  
 Pitot#: 0.85

Imp. #1: 

gross	572.9
tare	573.8
final	-0.9

Imp. #2: 

gross	611.4
tare	611.5
final	-0.1

Imp. #3: 

gross	480.7
tare	480.9
final	-0.2

Imp. #4: 

gross	632.3
tare	625.2
final	7.1

Total 5.9

Probe blank - ml  
 Probe rinse 200 ml

Solution blank DI  
 Solution blank Acetone

Filter No: F5,X43,X44  
 Filter Tare wt.           

	#	date
Solution Container		
Solution Container		

Sample Vol: 

start	150.0	ml	
Imp#1	finsh	149.1	ml

  
 Amount Gained: -0.9 ml

Sample Vol: 

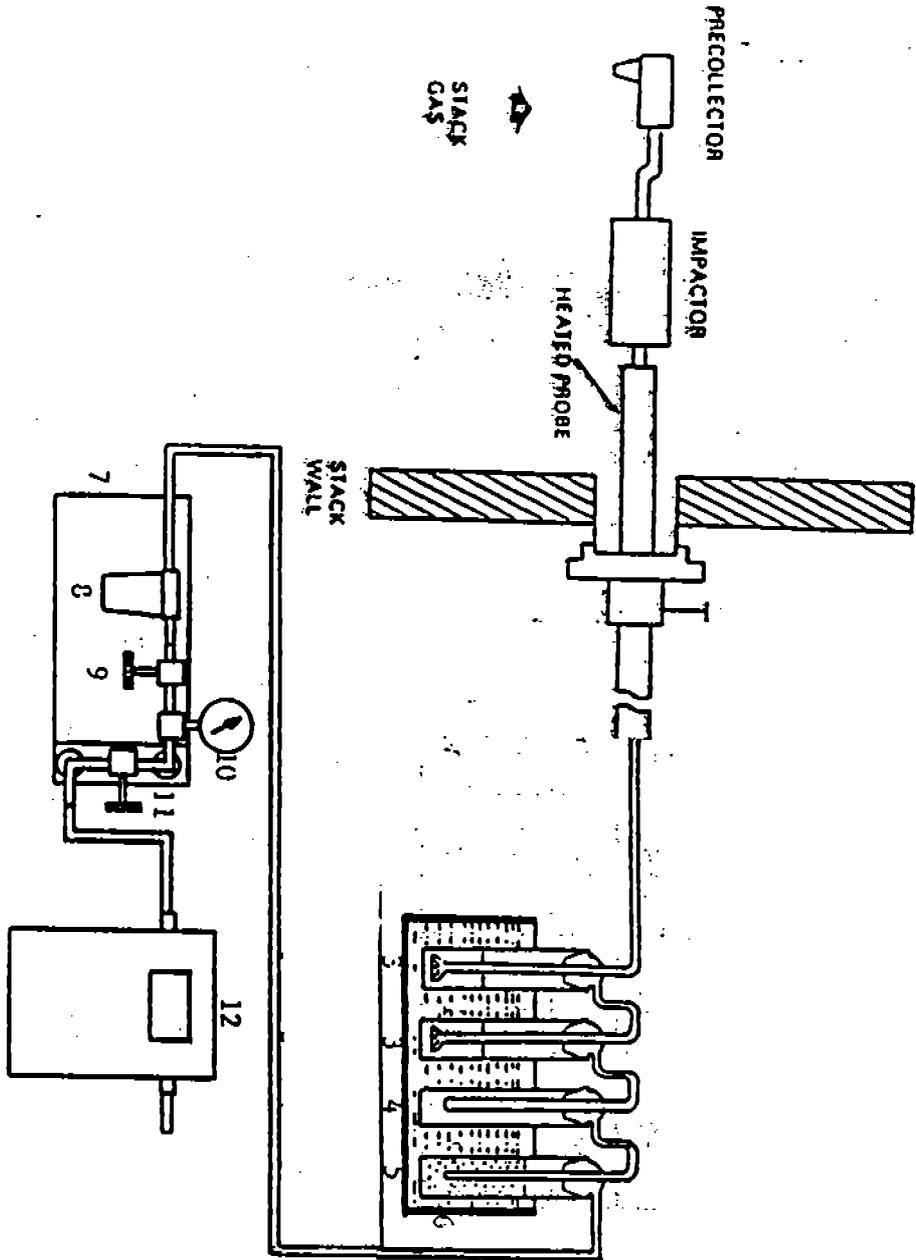
start	150.0	ml	
Imp #2	finsh	149.9	ml

  
 Amount Gained: -0.1 ml

Total Vol #1 #2 & Rinse 400.0 ml

Comments: \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_

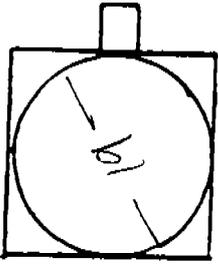
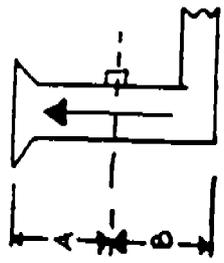
PM-10 PARTICULATE SAMPLING TRAIN



- 1. Stack Wall
- 2. Probe
- 3. Impinger with 100 ml of H<sub>2</sub>O
- 4. Empty Bubbler
- 5. Bubbler with Silica Gel
- 6. Ice Bath
- 7. Sealed Pump (Leak Free)
- 8. Filter for Pump
- 9. Metering Valve
- 10. Vacuum Gauge
- 11. By-pass Valve
- 12. Temperature Compensated Dry Gas Meter

**VII. RAW DATA**

PLANT: County Line Giv  
 LOCATION: Harshad  
 COUNTY: Kings  
 UNIT: Morte  
 DATE: 12/4/90  
 RUN NO./METHOD: 1A ~ Part  
 COLD BOX NO.: 5  
 METER BOX NO.: DE  
 METER FACTOR: L0231 AH0 = 2.1201  
 PITOT #/FACTOR: 7 ~ .8500  
 PYROMETER #: T-5  
 MAGNEHELIC FACTOR: ΔP 1.005 ΔH 0.995



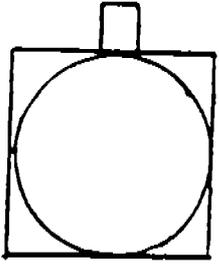
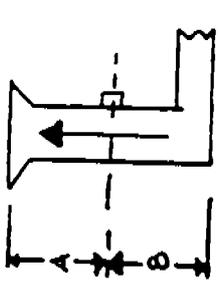
FILTER NO. D-24  
 AMBIENT TEMP.: 44  
 BARAMETRIC PRESS., IN. HG.: 30.21  
 ASSUMED MOISTURE: 57  
 HEATER BOX SETTING: 5  
 PROBE LENGTH, FT.: 5  
 NOZZLE DIAMETER, IN.: .223  
 PROBE HEATER SETTING:  
 APPROX. WIND VEL., MPH: calm  
 SAMPLE BOX TEMP., (F):  
 STATIC PRESSURE: -.15 "H2O  
 OFFSET: 0 in. PORT DIA.: 3 in. (M / )

TRAVERSE POINT NUMBER	DISTANCE INCHES	O2 (%)	CO2 (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY IN. H2O		PRESSURE DIFF ORIFICE METER (ΔH) IN. H2O	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GAS METER		PUMP VACUUM IN. HG.	TEMP. LAST IMPINGING (F)
						ΔP	ΔP			INLET (Tm),	OUTLET (Tm)		
1				3:55	55	.45		1.28	474.862	45	44		
2				3	55	.40		1.70	476.5	47	45		
3				6	55	.40		1.71	478.5	50	45		
4				9	56	.65		1.85	480.5	52	46		
5				12	56	.65		1.85	482.4	57	48	10	
6				18	56	.60		1.71	484.5	59	49		
7				18	56	.50		1.44	486.5	61	49		
8				21	57	.50		1.44	488.5	62	49		
9				24	59	.50		1.44	490.3	66	52		
10				27	60	.55		1.59	492.1	67	53		
11				30	61	.55		1.59	494.1	70	53		
12				33	61	.55		1.59	495.9	71	53		
				30					497.8				
AVERAGE													

PITOT LEAK CHECK:  
 BEFORE: TOP ΔP = 3.1 BOTTOM ΔP = 3.6  
 AFTER: TOP ΔP = 3.2 BOTTOM ΔP = 3.6  
 COMMENTS: PURGE

SAMPLE TRAIN LEAK:  
 BEFORE: 5.005 CRM@ 15 IN. HG.  
 AFTER: CRM@ IN. HG.

PLANT: County Line Gin  
 LOCATION: \_\_\_\_\_  
 COUNTY: \_\_\_\_\_  
 UNIT: Mo6  
 DATE: 12/4/90  
 RUN NO./METHOD: 131 Paint  
 COLD BOX NO.: \_\_\_\_\_  
 METER BOX NO.: \_\_\_\_\_  
 METER FACTOR: \_\_\_\_\_  
 PITOT #/ FACTOR: \_\_\_\_\_  
 PYROMETER #: \_\_\_\_\_  
 MAGNEHELIC FACTOR:  $\Delta P$  \_\_\_\_\_  $\Delta H$  \_\_\_\_\_



FILTER NO.: \_\_\_\_\_  
 AMBIENT TEMP.: \_\_\_\_\_  
 BAROMETRIC PRESS., IN. HG.: \_\_\_\_\_  
 ASSUMED MOISTURE: \_\_\_\_\_  
 HEATER BOX SETTING: \_\_\_\_\_  
 PROBE LENGTH, FT.: \_\_\_\_\_  
 NOZZLE DIAMETER, IN.: 22.3  
 PROBE HEATER SETTING: \_\_\_\_\_  
 APPROX. WIND VEL., MPH: \_\_\_\_\_  
 SAMPLE BOX TEMP., (F): \_\_\_\_\_  
 STATIC PRESSURE: \_\_\_\_\_ "H<sub>2</sub>O"  
 OFFSET: \_\_\_\_\_ in. PORT DIA.: \_\_\_\_\_ in. ( M / - )

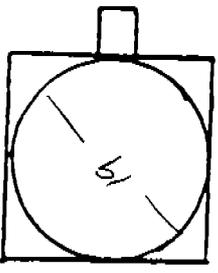
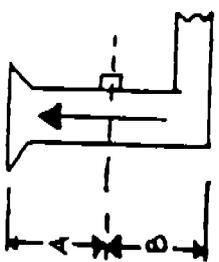
TRAVERSE POINT NUMBER	DISTANCE INCHES	O <sub>2</sub> (%)	CO <sub>2</sub> (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY IN. H <sub>2</sub> O		PRESSURE DIFF ORIFICE METER (ΔH) IN. H <sub>2</sub> O	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GAS METER		PUMP VACUUM IN. HG.	TEMP. LAST IMPINGER (F)
						ΔP	√ΔP			INLET (Tm), (TM)	OUTLET (TM)		
1				9:37	0	41	.35	1.01	497.8	60	60		
2				3	62	42	.40	1.15	499.4	70	58		
3				6	62	42	.40	1.15	501.0	73	60		
4				9	63	42	.42	1.23	502.7	73	60		
5				12	64	43	.43	1.25	504.4	73	61		
6				15	64	44	.45	1.31	506.1	74	63		
7				18	64	44	.55	1.41	507.9	75	63		
8				21	64	44	.60	1.46	509.8	76	63		
9				24	64	44	.60	1.46	511.8	76	63		
10				27	64	44	.67	1.46	513.8	79	63		
11				30	65	44	.65	1.40	516.0	80	64		
12				33	64	44	.72	2.13	518.1	80	64	10	
12				36					520.300				
AVERAGE													
PITOT LEAK CHECK:													
BEFORE:	TOP ΔP =												SAMPLE TRAIN LEAK:
AFTER:	ΔP =												IN. HG.
	TOP ΔP =												IN. HG.
	ΔP =												
COMMENTS:													PURGE

BEFORE: TOP ΔP = \_\_\_\_\_  
 ΔP = \_\_\_\_\_  
 AFTER: TOP ΔP = \_\_\_\_\_  
 ΔP = \_\_\_\_\_

BEFORE: BOTTOM ΔP = \_\_\_\_\_  
 ΔP = \_\_\_\_\_  
 AFTER: BOTTOM ΔP = \_\_\_\_\_  
 ΔP = \_\_\_\_\_

BEFORE: \_\_\_\_\_ IN. HG.  
 AFTER: \_\_\_\_\_ IN. HG.

PLANT: County Line Grain  
 LOCATION: Hanford  
 COUNTY: Kings  
 UNIT: Note  
 DATE: 12/4/90  
 RUN NO./METHOD: 2A ~ Part  
 COLD BOX NO.: 10  
 METER BOX NO.: BE  
 METER FACTOR: 1.0231  $\Delta H_0 = 2.1201$   
 PITOT #/FACTOR: 7 - 0.8500  
 PYROMETER #: \_\_\_\_\_  
 MAGNETIC FACTOR:  $\Delta P 1.005$   $\Delta H 0.992$



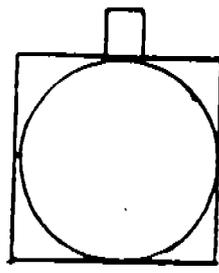
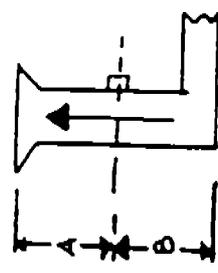
FILTER NO. D-25  
 AMBIENT TEMP.: 65  
 BAROMETRIC PRESS., IN. HG.: 30.21  
 ASSUMED MOISTURE: 57.0  
 HEATER BOX SETTING: \_\_\_\_\_  
 PROBE LENGTH, FT.: 51  
 NOZZLE DIAMETER, IN.: 203  
 PROBE HEATER SETTING: \_\_\_\_\_  
 APPROX. WIND VEL., MPH: calm  
 SAMPLE BOX TEMP., (F): \_\_\_\_\_  
 STATIC PRESSURE: -15 "H2O  
 OFFSET: \_\_\_\_\_ in. PORT DIA.: 3 in. ( M / )

TRAVERSE POINT NUMBER	DISTANCE INCHES	O2 (%)	CO2 (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY IN. H2O		PRESSURE DIFF ORIFICE METER ( $\Delta H$ ) IN. H2O	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GAS METER		PUMP VACUUM IN. HG.	TEMP. LAST IMPINGER (F)
						$\Delta P$	$\Delta P$			INLET (Tm),	OUTLET (TM)		
1				10.46	64	.45		1.36	520.867	64	64		
2				2.5	68	.40		1.15	522.4	68	64		
3				5	69	.40		1.15	524.0	69	64		
4				7.2	70	.65		1.07	525.7	75	64		
5				10	72	.65		1.07	527.6	76	64		
6				12.5	73	.60		1.18	529.4	82	68		
7				15	74	.50		1.46	531.1	82	68		
8				17.5	75	.50		1.45	532.6	83	68		
9				20	75	.50		1.49	534.1	84	68		
10				22.5	75	.55		1.59	535.7	86	69		
11				25	76	.55		1.59	537.2	90	72		
12				27.5	79	.55		1.59	538.8	91	73		
AVERAGE				30					540.4				

PITOT LEAK CHECK:  
 BEFORE: TOP  $\Delta P = 3.2$  BOTTOM  $\Delta P = 3.5$   
 AFTER: TOP  $\Delta P = 3.2$  BOTTOM  $\Delta P = 3.5$   
 SAMPLE TRAIN LEAK:  
 BEFORE: 2,002 CFM@ 15 IN. HG.  
 AFTER: 2,005 CFM@ 15 IN. HG.  
 COMMENTS: \_\_\_\_\_ PURGE \_\_\_\_\_

23265  
 007

PLANT: County Line Gas  
 LOCATION: \_\_\_\_\_  
 COUNTY: \_\_\_\_\_  
 UNIT: Mojo  
 DATE: 12/4/96  
 RUN NO/METHOD: 2B - Part  
 COLD BOX NO.: \_\_\_\_\_  
 METER BOX NO.: \_\_\_\_\_  
 METER FACTOR: \_\_\_\_\_  
 PITOT #/ FACTOR: \_\_\_\_\_  
 PYROMETER #: \_\_\_\_\_  
 MAGNETIC FACTOR:  $\Delta P$   $\Delta H$

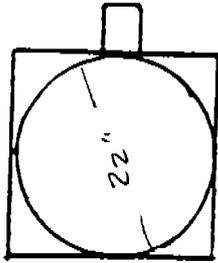
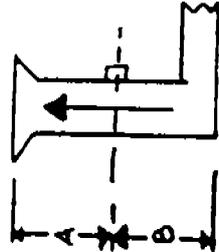


FILTER NO.: \_\_\_\_\_  
 AMBIENT TEMP.: \_\_\_\_\_  
 BAROMETRIC PRESS., IN. HG.: \_\_\_\_\_  
 ASSUMED MOISTURE: \_\_\_\_\_  
 HEATER BOX SETTING: \_\_\_\_\_  
 PROBE LENGTH, FT.: \_\_\_\_\_  
 NOZZLE DIAMETER, IN.: 2.23  
 PROBE HEATER SETTING: \_\_\_\_\_  
 APPROX. WIND VEL., MPH: \_\_\_\_\_  
 SAMPLE BOX TEMP., (F): \_\_\_\_\_  
 STATIC PRESSURE: \_\_\_\_\_  
 OFFSET: \_\_\_\_\_ in.  $\Delta P$   $\Delta H$   
 PORT DIA.: 2 in. (M / )

TRAVERSE POINT NUMBER	DISTANCE INCHES	O2 (%)	CO2 (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY IN. H2O		PRESSURE DIFF ORIFICE METER ( $\Delta H$ )	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GAS METER		PUMP VACUUM IN. HG.	TEMP. LAST IMPINGER (F)
						$\Delta P$	$\Delta P$			INLET (Tm)	OUTLET (Tm)		
1				11:10	76	.35		1.01	540.4	76	76		
2				2.5	76	.40		1.14	541.7	85	76		
3				5	74	.40		1.17	543.2	88	76		
4				7.5	74	.42		1.22	544.5	90	77		
5				10	76	.43		1.25	545.9	93	79		
6				12.5	74	.45		1.22	547.4	94	80		
7				15	77	.55		1.62	548.9	94	79		
8				17.5	77	.60		1.76	550.5	95	80		
9				20	77	.60		1.76	552.1	97	80		
10				22.5	77	.67		1.96	553.8	97	81		
11				25	77	.65		1.91	555.6	98	81		
12				27.5	77	.72		2.11	557.4	99	81		
				30					559.252	99	81		
AVERAGE									38.985	161.3			
PITOT LEAK CHECK:													
BEFORE: TOP $\Delta P$ = _____ BOTTOM $\Delta P$ = _____													
AFTER: TOP $\Delta P$ = _____ BOTTOM $\Delta P$ = _____													
SAMPLE TRAIN LEAK: _____ IN. HG.													
BEFORE: _____ IN. HG.													
AFTER: _____ IN. HG.													
COMMENTS: _____													
PURGE _____													

83

PLANT: County Line Gin  
 LOCATION: Hartford  
 COUNTY: Kings  
 UNIT: Unit 1 Trap  
 DATE: 12/4/90  
 RUN NO./METHOD: 1A - Part  
 COLD BOX NO.: 5  
 METER BOX NO.: BE  
 METER FACTOR: 1.0231,  $\Delta H = 2.1701$   
 PITOT #/FACTOR: 7 - 1.8500  
 PYROMETER #: 7-5  
 MAGNEHELIC FACTOR:  $\Delta P$  1.005  $\Delta H$  0.955



FILTER NO. D-26  
 AMBIENT TEMP.: 75  
 BARAMETRIC PRESS., IN. HG.: 30.1  
 ASSUMED MOISTURE: 5%  
 HEATER BOX SETTING:  
 PROBE LENGTH, FT.: 51  
 NOZZLE DIAMETER, IN.: 1.273  
 PROBE HEATER SETTING:  
 APPROX. WIND VEL., MPH: calm  
 SAMPLE BOX TEMP., (F):  
 STATIC PRESSURE: 1.10 "H2O  
 OFFSET: 0 in. PORT DIA.: 3 in. (M / -)

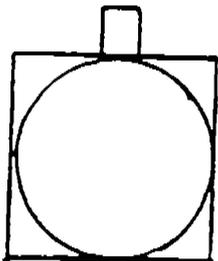
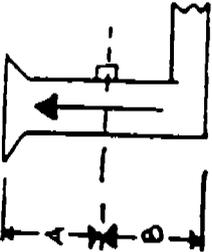
TRAVERSE POINT NUMBER	DISTANCE INCHES	O2 (%)	CO2 (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY HEAD IN. H2O		PRESSURE DIFF ORIFICE METER ( $\Delta H$ ) IN. H2O	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GAS METER		PUMP VACUUM IN. HG.	TEMP. LAST IMPINGER (F)
						$\Delta P$	$\sqrt{\Delta P}$			INLET (Tm),	OUTLET (Tm)		
1				1:10	98	.40		1.10	559.532	68	67		
2				3	97	.42		1.10	561.2	72	70		
3				6	97	.45		1.25	562.8	76	73		
4				9	98	.45		1.25	564.6	78	71	8	
5				12	99	.45		1.25	566.3	80	69		
6				15	100	.41		1.14	568.0	82	70		
7				18	100	.30		.83	569.7	84	71		
8				21	101	.30		.83	571.2	85	73		
9				24	102	.32		.90	572.6	88	74		
10				27	102	.38		1.07	574.1	90	75		
11				30	102	.38		1.07	575.7	91	76		
12				33	102	.38		1.07	577.3	92	77		
12				36					578.9				
AVERAGE									456.3				

PITOT LEAK CHECK:  
 BEFORE: TOP  $\Delta P = 3.1$  BOTTOM  $\Delta P = 3.7$   
 AFTER: TOP  $\Delta P = 3.2$  BOTTOM  $\Delta P = 3.1$   
 TOP  $\Delta P = 3.0$  BOTTOM  $\Delta P = 3.8$   
 $\Delta P = 3.0$   $\Delta P = 3.8$

SAMPLE TRAIN LEAK:  
 BEFORE: CRM@ 17 IN. HG.  
 AFTER: CRM@ 15 IN. HG.

COMMENTS: PURGE

PLANT: \_\_\_\_\_  
 LOCATION: \_\_\_\_\_  
 COUNTY: \_\_\_\_\_  
 UNIT: Lint Trap  
 DATE: 12/4/50  
 RUN NO./METHOD: 12-Part  
 COLD BOX NO.: \_\_\_\_\_  
 METER BOX NO.: \_\_\_\_\_  
 METER FACTOR: \_\_\_\_\_  
 PITOT #/FACTOR: \_\_\_\_\_  
 PYROMETER #: \_\_\_\_\_  
 MAGNETIC FACTOR:  $\Delta P$  \_\_\_\_\_  $\Delta H$  \_\_\_\_\_



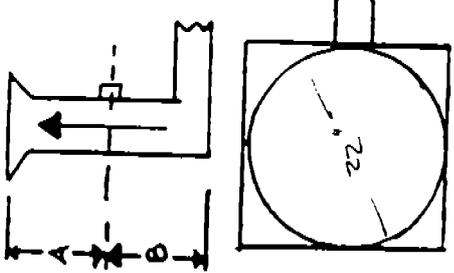
FILTER NO.: \_\_\_\_\_  
 AMBIENT TEMP.: \_\_\_\_\_  
 BAROMETRIC PRESS., IN. HG.: \_\_\_\_\_  
 ASSUMED MOISTURE: \_\_\_\_\_  
 HEATER BOX SETTING: \_\_\_\_\_  
 PROBE LENGTH, FT.: \_\_\_\_\_  
 NOZZLE DIAMETER, IN.: .223  
 PROBE HEATER SETTING: \_\_\_\_\_  
 APPROX. WIND VEL., MPH: \_\_\_\_\_  
 SAMPLE BOX TEMP., (F): \_\_\_\_\_  
 STATIC PRESSURE: \_\_\_\_\_  
 OFFSET: \_\_\_\_\_ in.  $\Delta H_2O$  \_\_\_\_\_ in. PORT DIA.: \_\_\_\_\_ in. ( M / - )

TRAVERSE POINT NUMBER	DISTANCE INCHES	O2 (%)	CO2 (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY IN. H2O		PRESSURE DIFF ORIFICE METER ( $\Delta H$ ) IN. H2O	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GASMETER		PUMP VACUUM IN. HG.	TEMP. LAST IMPINGER (F)
						$\Delta P$	$\sqrt{\Delta P}$			INLET (Tm),	OUTLET (Tm)		
1				1:55	110	.26		.71	578.9	78	78		
2				2	110	.28		.76	500.3	81	78		
3				6	111	.30		.82	501.7	89	80		
4				9	111	.30		.92	503.2	89	80		
5				12	111	.30		.82	584.5	91	81		
6				15	111	.30		.82	586.6	92	81		
7				18	112	.30		.82	587.4	93	83		
8				21	112	.32		.88	588.9	93	81		
9				24	112	.35		.91	590.4	95	82		
10				27	112	.38		1.03	591.9	95	82	8	
11				30	111	.38		1.05	<del>593.4</del>	95	82		
12				33	110	.38		1.05	593.4	96	83		
36				36					595.022				
AVERAGE		20.9	0.05	72	105.5		0.585	0.979	735.530	81.6			

PITOT LEAK CHECK:  
 BEFORE: TOP  $\Delta P$  = \_\_\_\_\_ BOTTOM  $\Delta P$  = \_\_\_\_\_  
 AFTER: TOP  $\Delta P$  = \_\_\_\_\_ BOTTOM  $\Delta P$  = \_\_\_\_\_

SAMPLE TRAIN LEAK:  
 BEFORE: \_\_\_\_\_ IN. HG.  
 AFTER: \_\_\_\_\_ IN. HG.  
 COMMENTS: \_\_\_\_\_ PURGE \_\_\_\_\_

PLANT: County Line Gin  
 LOCATION: Hatch  
 COUNTY: Kings  
 UNIT: Unit 1 trap  
 DATE: 12/4/50  
 RUN NO./METHOD: 2A - Part  
 COLD BOX NO.: DE  
 METER BOX NO.: 1.0231  
 METER FACTOR: ΔH = 2.1201  
 PITOT #/ FACTOR: 7 ~ 0.000  
 PYROMETER #: \_\_\_\_\_  
 MAGNETIC FACTOR: ΔP 1.005 ΔH 0.975

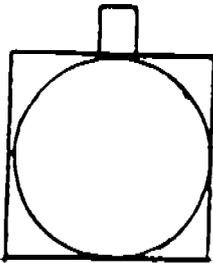
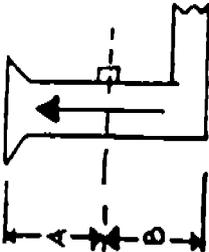


FILTER NO. D-22  
 AMBIENT TEMP.: 75  
 BAROMETRIC PRESS., IN. HG.: 30.1  
 ASSUMED MOISTURE: 5%  
 HEATER BOX SETTING: \_\_\_\_\_  
 PROBE LENGTH, FT.: 5'  
 NOZZLE DIAMETER, IN.: .223  
 PROBE HEATER SETTING: \_\_\_\_\_  
 APPROX. WIND VEL., MPH: calm  
 SAMPLE BOX TEMP., (F): \_\_\_\_\_  
 STATIC PRESSURE: -.10 \*H2O  
 OFFSET: 0 in. PORT DIA.: 3 in. (M / -)

TRAVERSE POINT NUMBER	DISTANCE INCHES	O2 (%)	CO2 (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY HEAD IN. H2O		PRESSURE DIFF ORIFICE METER (ΔH) IN. H2O	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GAS METER		PUMP VACUUM IN. HG.	TEMP. LAST IMPINGER (F)
						ΔP	√ΔP			INLET (Tm),	OUTLET (Tm)		
1				2:51	110	.40		1.09	595.201	75	75		
2				3	110	.43		1.17	596.7	81	75		
3				6	110	.43		1.17	596.4	82	75		
4				9	111	.45		1.23	600.1	87	75		
5				12	111	.45		1.23	601.9	87	75		
6				15	118	.40		1.10	603.9	99	77		
7				18	109	.30		.83	605.2	90	77		
8				21	110	.30		.83	606.7	91	78		
9				24	110	.35		.97	608.1	91	78		
10				27	96	.38		1.05	609.7	93	73		
11				30	96	.38		1.06	611.2	90	73		
12				33	96	.38		1.05	612.9	89	77		
				36					614.5				
AVERAGE													

PITOT LEAK CHECK: BEFORE: TOP ΔP = 3.6 ΔP = 3.6 AFTER: TOP ΔP = 3.8 ΔP = 3.8  
 BOTTOM ΔP = 3.2 ΔP = 3.2 BOTTOM ΔP = 3.1 ΔP = 3.1  
 SAMPLE TRAIN LEAK: BEFORE = 2.005 CFM @ 15 IN. HG. AFTER = 2.005 CFM @ 15 IN. HG.  
 COMMENTS: \_\_\_\_\_ PURGE \_\_\_\_\_

PLANT: \_\_\_\_\_  
 LOCATION: \_\_\_\_\_  
 COUNTY: \_\_\_\_\_  
 UNIT: Lind Trap  
 DATE: 12/4/90  
 RUN NO./METHOD: 2B - Part  
 COLD BOX NO.: \_\_\_\_\_  
 METER BOX NO.: \_\_\_\_\_  
 METER FACTOR: \_\_\_\_\_  
 PITOT #/FACTOR: \_\_\_\_\_  
 PYROMETER #: \_\_\_\_\_  
 MAGNEHELIC FACTOR:  $\Delta P$  \_\_\_\_\_  $\Delta H$  \_\_\_\_\_

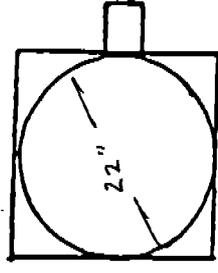
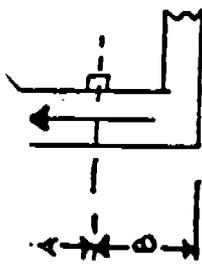


FILTER NO. \_\_\_\_\_  
 AMBIENT TEMP.: \_\_\_\_\_  
 BARAMETRIC PRESS., IN. HG.: \_\_\_\_\_  
 ASSUMED MOISTURE: \_\_\_\_\_  
 HEATER BOX SETTING: \_\_\_\_\_  
 PROBE LENGTH, FT.: \_\_\_\_\_  
 NOZZLE DIAMETER, IN.: .223  
 PROBE HEATER SETTING: \_\_\_\_\_  
 APPROX. WIND VEL., MPH: \_\_\_\_\_  
 SAMPLE BOX TEMP., (F): \_\_\_\_\_  
 STATIC PREASURE: \_\_\_\_\_ \*H2O  
 OFFSET: \_\_\_\_\_ in. PORT DIA.: \_\_\_\_\_ in. ( M / - )

TRAVERSE POINT NUMBER	DISTANCE INCHES	O2 (%)	CO2 (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY HEAD IN. H2O		PRESSURE DIFF ORIFICE METER ( $\Delta H$ ) IN. H2O	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GAS METER		PUMP VACUUM IN. HG.	TEMP. LAST IMPINGER (F)
						$\Delta P$	$\sqrt{\Delta P}$			INLET (Tm), (Tm)	OUTLET (Tm)		
1				3:58	96	.125	.692	72	614.5	72	72		
2				3	97	.128	.774	75	615.9	75	73		
3				4	97	.13	.83	80	617.3	80	73		
4				9	98	.13	.84	85	618.8	85	75		
5				12	98	.13	.84	88	620.3	88	76		
6				15	99	.128	.79	91	621.7	91	76		
7				18	99	.129	.81	91	623.2	91	76		
8				21	102	.135	.89	92	624.6	92	87		
9				24	101	.137	1.05	94	626.2	94	79		
10				27	98	.14	1.13	94	627.9	94	81		
11				30	97	.142	1.19	95	629.5	95	79		
12				33	97	.145	1.27	96	631.2	96	80		
	ZERO SPAN			36					632.938				
AVERAGE			28%	0.05	102.4		0.598	0.999	37.737	90.9			

PITOT LEAK CHECK:  
 BEFORE: TOP  $\Delta P$  = \_\_\_\_\_ BOTTOM  $\Delta P$  = \_\_\_\_\_  
 AFTER: TOP  $\Delta P$  = \_\_\_\_\_ BOTTOM  $\Delta P$  = \_\_\_\_\_  
 SAMPLE TRAIN LEAK:  
 BEFORE: CRM@ \_\_\_\_\_ IN. HG.  
 AFTER: CRM@ \_\_\_\_\_ IN. HG.  
 COMMENTS: \_\_\_\_\_ PURGE \_\_\_\_\_

PL : 36 4 2 6  
 LOCATION: Hay Field  
 COUNTY: King  
 UNIT: Suction  
 DATE: 12/3/90  
 RUN NO/METHOD: 1A Meth 5:  
 COLD BOX NO.: 2  
 METER BOX NO.: D  
 METER FACTOR: .9685  
 PITOT #/FACTOR: 7 ~ 0.8500  
 PYROMETER #: 7-5  
 MAGNEHELIC FACTOR: ΔP 1.008 ΔH .952



FILTER NO. D-20  
 AMBIENT TEMP.: 40 F  
 BARAMETRIC PRESS., IN. HG.: 30.27  
 ASSUMED MOISTURE: 5%  
 HEATER BOX SETTING:  
 PROBE LENGTH, FT.: 5  
 NOZZLE DIAMETER, IN.: .298  
 PROBE HEATER SETTING:  
 APPROX. WIND VEL., MPH:  
 SAMPLE BOX TEMP., (F):  
 STATIC PRESSURE: -.03 \*H2O  
 OFFSET: 9 in. PORT DIA.: 3 in. (M / F)

TRAVERSE POINT NUMBER	DISTANCE INCHES	O2 (%)	CO2 (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY IN. H2O		PRESSURE DIFF. ORIFICE METER (ΔH) IN. H2O	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GAS METER		PUMP VACUUM IN. HG.	TEM. LAST IMPINGER (F)
						ΔP	√ΔP			INLET (Tm),	OUTLET (Tm)		
<i>Pitot</i>													
32760 1		20.9	0.1	9:30	72	.120		1.02	319.959	49	49		
2				3	73	.125		1.07	321.5	54	50		
3				6	73	.110		.94	323.1	60	53		
4				9	73	.140		1.20	324.7	64	51	7	
5				12	74	.140		1.37	326.4	70	54	8	
6				15	74	.20		1.75	328.3	72	54	9	
7				18	74	.21		1.84	330.1	74	57		
8				21	74	.21		1.84	332.1	75	57		
9				24	75	.21		1.84	334.2	77	60	12	
10				27	75	.195		1.71	336.4	77	60		
11				30	75	.185		1.62	338.5	80	65		
12				33	75	.17		1.51	340.3	81	65		
	ZERO			36					342.3				
	SPAN					.170							
AVERAGE													

PITOT LEAK CHECK:  
 BEFORE: TOP ΔP = 3.1 BOTTOM ΔP = 3.5  
 ΔP = 3.1 ΔP = 3.5  
 AFTER: TOP ΔP = 4.2 BOTTOM ΔP = 3.7  
 ΔP = 4.2 ΔP = 3.7

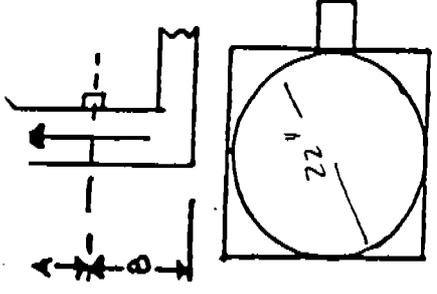
SAMPLE TRAIN LEAK:  
 BEFORE = 2.002 IN. HG.  
 AFTER = 2.005 IN. HG.

COMMENTS: PURGE

$M_d = 28.852$   
 $M_w = 28.309$   
 $AP_{60} = .164$   
 $D_u \text{ ideal} = .325$



LOCATION: Hayfield  
 COUNTY: Kings  
 UNIT: Suction  
 DATE: 12/3/90  
 RUN NO/METHOD: 24 ~ Part\*  
 COLD BOX NO.: 10  
 METER BOX NO.: D  
 METER FACTOR: .9685 ΔHC = 2.155  
 PITOT #/FACTOR: 7 ~ .8500  
 PYROMETER #: T-5  
 MAGNEHELIC FACTOR: ΔP 1.008 ΔH .952



FILTER NO. D-21  
 AMBIENT TEMP.: 52  
 BAROMETRIC PRESS., IN. HG.: 30.27  
 ASSUMED MOISTURE: 5%  
 HEATER BOX SETTING:  
 PROBE LENGTH, FT.: 5  
 NOZZLE DIAMETER, IN.: .298  
 PROBE HEATER SETTING:  
 APPROX. WIND VEL., MPH:  
 SAMPLE BOX TEMP., (F):  
 STATIC PRESSURE: -.03 "H2O  
 OFFSET: φ in. PORT DIA.: 3 in. (M / F)

TRAVERSE POINT NUMBER	DISTANCE INCHES	O2 (%)	CO2 (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY IN. H2O		PRESSURE DIFF ORIFICE METER (ΔH) IN. H2O	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GAS METER		PUMP VACUUM IN. HG.	TEL. LAST IMPINGER (F)
						ΔP	√ΔP			INLET (Tm),	OUTLET (Tm)		
1				11:00	82	.115		1.00	364.918	68	67		
2				2.5	82	.135		1.18	366.5	79	67		
3				5	87	.155		1.35	367.7	76	67		
4				7.5	87	.170		1.49	369.4	81	67		
5				10	84	.175		1.53	370.9	86	67		
6				12.5	85	.180		1.59	372.4	86	67		
7				15	84	.185		1.64	374.3	87	68		
8				17.5	84	.185		1.64	375.8	86	67		
9				20	84	.165		1.46	377.5	88	70		
10				22.5	84	.155		1.37	379.1	88	70		
11				25	86	.145		1.28	380.8	89	70		
12				27.5	85	.140		1.24	382.1	89	71		
30									389.5				
AVERAGE													

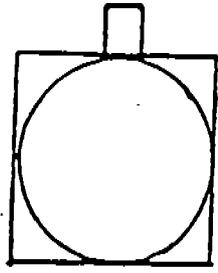
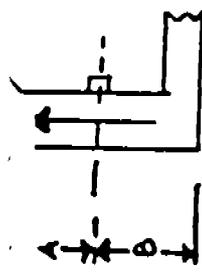
PTOT LEAK CHECK:  
 BEFORE: TOP ΔP = 3.6 BOTTOM ΔP = 3.2  
 ΔP = 2.4 ΔP = 2.2  
 AFTER: TOP ΔP = 7.5 BOTTOM ΔP = 7.4  
 ΔP = 3.5 ΔP = 3.4

SAMPLE TRAIN LEAK:  
 BEFORE = 2.002 CRM@ 15 IN. HG.  
 AFTER = 1.005 CRM@ 15 IN. HG.

COMMENTS: PURGE

06

LOCATION: 45 121  
 COUNTY: Suction  
 UNIT: 12/3/90  
 DATE: 28 - Part  
 RUN NO. METHOD: 28 - Part  
 COLD BOX NO.:  
 METER BOX NO.:  
 METER FACTOR:  
 PITOT #/ FACTOR:  
 PYROMETER #:  
 MAGNETIC FACTOR:  $\Delta P$   $\Delta H$

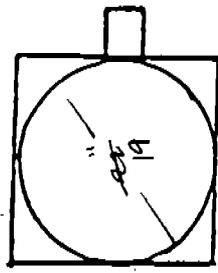
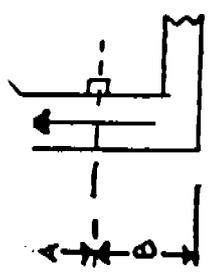


FILTER NO. D-21  
 AMBIENT TEMP.:  
 BAROMETRIC PRESS. IN. HG.:  
 ASSUMED MOISTURE:  
 HEATER BOX SETTING:  
 PROBE LENGTH, FT.:  
 NOZZLE DIAMETER, IN.:  
 PROBE HEATER SETTING:  
 APPROX. WIND VEL. MPH:  
 SAMPLE BOX TEMP., (F):  
 STATIC PRESSURE:  $^{\circ}H_2O$   
 OFFSET: in. PORT DIA.: in. (M / F)

TRAVERSE POINT NUMBER	DISTANCE INCHES	O2 (%)	CO2 (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY IN. H2O		PRESSURE DIFF ORIFICE METER (ΔH) IN. H2O	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GAS METER		PUMP VACUUM IN. HG.	TEA LAST IMPINGER (F)
						ΔP	ΔP			INLET (Tm),	OUTLET (Tm)		
1				11:40	85	.120		1.04	383.3	76	73		
2				12.5	85	.105		1.09	305.0	80	71		
3				5	85	.110		.96	386.3	86	71		
4				7.5	85	.135		1.18	418.38716	88	72		
5				10	85	.165		1.45	389.1	89	72		
6				12.5	85	.285		1.9	390.7	91	72		
7				19	85	.21		1.85	392.4	92	76	6	
8				17.5	85	.21		1.85	394.1	91	75		
9				20	85	.21		1.85	395.9	92	76		
10				22.5	82	.190	Q1A	1.63	397.9	64	64		
11				25	84	.190		1.64	399.4	70	65		
12				22.5	84	.165		1.43	401.1	73	64		
13				40					402.641				
AVERAGE									37.127				
PITOT LEAK CHECK:									37.127				
BEFORE:													
AFTER:													

SAMPLE TRAIN LEAK:  
 BEFORE: 76.3 IN. HG.  
 AFTER: 76.3 IN. HG.  
 COMMENTS: CRM@  
CRM@  
FURGE

PL : C by 19  
 LOCATION: Hayford  
 COUNTY: Kings  
 UNIT: #1 Dwyer  
 DATE: 12/9/50  
 RUN NO. METHOD: 1A ~ Pitot  
 COLD BOX NO.: 5  
 METER BOX NO.: D  
 METER FACTOR: 1.685, ΔH = 2.1055  
 PITOT #/ FACTOR: 7 ~ 2.500  
 PYROMETER #: 7-5  
 MAGNEHELC FACTOR: ΔP 1.008 ΔH 0.952



FILTER NO.: D-66  
 AMBIENT TEMP.: 65  
 BAROMETRIC PRESS., IN. HG.: 30.25  
 ASSUMED MOISTURE: 5%  
 HEATER BOX SETTING: —  
 PROBE LENGTH, FT.: 5  
 NOZZLE DIAMETER, IN.: .256  
 PROBE HEATER SETTING: —  
 APPROX. WIND VEL., MPH: Calman  
 SAMPLE BOX TEMP., (F): —  
 STATIC PRESSURE: -.06 H<sub>2</sub>O = -.004 H<sub>2</sub>  
 OFFSET: 0 in. PORT DIA.: 3 in. (M / F)

TRAVERSE POINT NUMBER	DISTANCE INCHES	O2 (%)	CO2 (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY IN. H2O		PRESSURE DIFF. ORIFICE METER (ΔH) IN. H2O	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GAS METER		PUMP VACUUM IN. HG.	TEI LAST IMPINGER (F)
						ΔP	ΔP			INLET (Tm)	OUTLET (Tm)		
1	30858			1:55	114	.17	.27	1.27	402.975	63	62		
2				3	115	.35	.28	1.32	404.8	64	61		
3				6	115	.28	.28	1.33	406.5	72	64	9	
4				9	117	.39	.28	1.33	408.3	75	62		
5				12	120		.215	1.31	410.2	79	63		
6				15	125		.285	1.34	412.1	82	66		
7				18	127		.30	1.43	413.9	85	67		
8				21	130		.31	1.47	415.7	87	68		
9				24	131		.315	1.49	417.5	89	69		
10				27	137		.30	1.47	419.5	90	71		
11				30	137		.285	1.37	421.3	91	72		
12				33	137		.285	1.33	423.2	91	73		
				36			<del>.28</del>		425.1				
AVERAGE							.287						

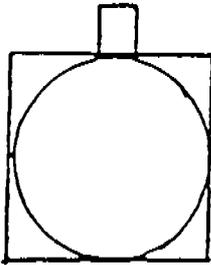
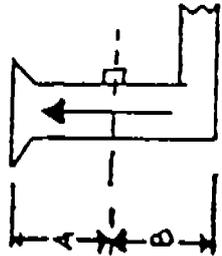
PITOT LEAK CHECK: BEFORE: TOP ΔP = 3.7 BOTTOM ΔP = 3.3  
 ΔP = 3.7 ΔP = 3.3  
 AFTER: TOP ΔP = 3.8 BOTTOM ΔP = 3.3  
 ΔP = 3.8 ΔP = 3.3

SAMPLE TRAIN LEAK: BEFORE: <.002 CRMG @ 15 IN. HG.  
 AFTER: <.002 CRMG @ 15 IN. HG.

COMMENTS: PURGE

$D_n = .287$

PLANT: County Line Grain  
 LOCATION: \_\_\_\_\_  
 COUNTY: \_\_\_\_\_  
 UNIT: #1 Drier  
 DATE: 12/3/90  
 RUN NO./METHOD: 1B ~ Test  
 COLD BOX NO.: \_\_\_\_\_  
 METER BOX NO.: \_\_\_\_\_  
 METER FACTOR: \_\_\_\_\_  
 PITOT #/FACTOR: \_\_\_\_\_  
 PYROMETER #: \_\_\_\_\_  
 MAGNETIC FACTOR:  $\Delta P$  \_\_\_\_\_  $\Delta H$  \_\_\_\_\_



FILTER NO. \_\_\_\_\_  
 AMBIENT TEMP.: \_\_\_\_\_  
 BAROMETRIC PRESS., IN. HG.: \_\_\_\_\_  
 ASSUMED MOISTURE: \_\_\_\_\_  
 HEATER BOX SETTING: \_\_\_\_\_  
 PROBE LENGTH, FT.: \_\_\_\_\_  
 NOZZLE DIAMETER, IN.: \_\_\_\_\_  
 PROBE HEATER SETTING: \_\_\_\_\_  
 APPROX. WIND VEL., MPH: \_\_\_\_\_  
 SAMPLE BOX TEMP., (F): \_\_\_\_\_  
 STATIC PRESSURE: \_\_\_\_\_ \*H2O  
 OFFSET: \_\_\_\_\_ in. PORT DIA.: \_\_\_\_\_ in. (M / F)

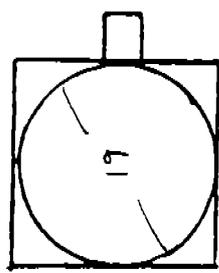
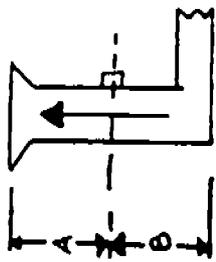
TRAVERSE POINT NUMBER	DISTANCE INCHES	O2 (%)	CO2 (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY IN. H2O		PRESSURE DIFF ORIFICE METER ( $\Delta H$ ) IN. H2O	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GAS METER		PUMP VACUUM IN. HG.	TEMP. LAST IMPINGER (F)
						$\Delta P$	$\Delta P$			INLET (Tm)	OUTLET (Tm)		
1				2:35	141	.285		1.32	425.1	77	76		
2				3	142	.30		1.40	426.9	88	76		
3				6	142	.30		1.41	428.8	90	79		
4				9	141	.31		1.45	430.6	91	80		
5				12	140	.315		1.48	432.5	91	80		
6				15	137	.315		1.48	434.4	93	80		
7				18	135	.30		1.41	436.5	93	80		
8				21	130	.28		1.31	438.3	94	80		
9				24	136	.215		1.29	440.1	95	80		
10				27	135	.21		1.27	441.9	96	80		
11				30	130	.26		1.22	439.9	97	80		
12				33	125	.26		1.22	445.6	97	81		
				36					447.352				
AVERAGE				72	136.4	.289	0.57	1.359	447.77	94.6			

PITOT LEAK CHECK: BEFORE: TOP  $\Delta P$  = \_\_\_\_\_ BOTTOM  $\Delta P$  = \_\_\_\_\_  
 AFTER: TOP  $\Delta P$  = \_\_\_\_\_ BOTTOM  $\Delta P$  = \_\_\_\_\_  
 SAMPLE TRAIN LEAK: BEFORE: \_\_\_\_\_ IN. HG.  
 AFTER: \_\_\_\_\_ IN. HG.  
 COMMENTS: \_\_\_\_\_  
 PURGE: \_\_\_\_\_

93

11 (#)

PLANT: County Line Grain  
 LOCATION: Headfield  
 COUNTY: Kings  
 UNIT: #1 Dryer  
 DATE: 12/3/50  
 RUN NO. METHOD: 2A ~ Part  
 COLD BOX NO.: 10  
 METER BOX NO.: D  
 METER FACTOR: 9685, APD = 2.1055  
 PITOT #/ FACTOR: 7 ~ .850  
 PYROMETER #: T.5  
 MAGNEHELIC FACTOR: ΔP 1.008 ΔH 0.952



FILTER NO.: D-23  
 AMBIENT TEMP.: 68  
 BARAMETRIC PRESS., IN. HG.: 30.25  
 ASSUMED MOISTURE: 5%  
 HEATER BOX SETTING: 5  
 PROBE LENGTH, FT.: 5  
 NOZZLE DIAMETER, IN.: .255  
 PROBE HEATER SETTING: 1  
 APPROX. WIND VEL., MPH: calm  
 SAMPLE BOX TEMP., (F): —  
 STATIC PRESSURE: -.06 \*H2O  
 OFFSET: 0 in. PORT DIA.: 3 in. (M / -)

TRAVERSE POINT NUMBER	DISTANCE INCHES	O2 (%)	CO2 (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY IN. H2O		PRESSURE DIFF ORIFICE METER (ΔH) IN. H2O	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GAS METER		PUMP VACUUM IN. HG.	TEMP. LAST IMPINGER (F)
						ΔP	√ΔP			INLET (Tm),	OUTLET (Tm)		
1				3.45	138	.27		1.25	447.442	77	77		
2				3	145	.28		1.28	449.2	76	70		
3				6	147	.28		1.28	451.0	80	70		
4				9	147	.28		1.28	452.8	80	71		
5				12	147	.295		1.27	454.4	85	73	4	
6				15	148	.27		1.24	456.3	87	70		
7				18	148	.30		1.40	458.1	89	71		
8				21	148	.315		1.65	459.8	89	72		
9				24	147	.315		1.65	461.8	90	73		
10				27	147	.285		1.32	464.0	92	73		
11				30	147	.285		1.32	465.8	93	74		
12				33	147	.285		1.32	467.6	94	75		
13				36									
AVERAGE													

PITOT LEAK CHECK:  
 BEFORE: TOP ΔP = 3.5 ΔP = 3.5  
 AFTER: TOP ΔP = 4.2 ΔP = 4.2

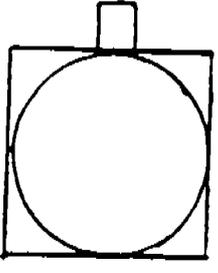
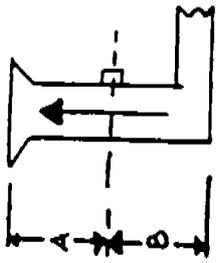
BOTTOM ΔP = 3.2 ΔP = 3.2  
 BOTTOM ΔP = 3.8 ΔP = 3.4

SAMPLE TRAIN LEAK:  
 BEFORE = 1.005 CFM @ 15 IN. HG.  
 AFTER = 1.005 CFM @ 15 IN. HG.

COMMENTS: PURGE

Hand # 320051  
 94

PLANT: Courby Linn Gin  
 LOCATION: \_\_\_\_\_  
 COUNTY: \_\_\_\_\_  
 UNIT: Dgas #1  
 DATE: 12/3/90  
 RUN NO./METHOD: 2B ~ Part  
 COLD BOX NO.: \_\_\_\_\_  
 METER BOX NO.: \_\_\_\_\_  
 METER FACTOR: \_\_\_\_\_  
 PITOT #/FACTOR: \_\_\_\_\_  
 PYROMETER #: \_\_\_\_\_  
 MAGNETIC FACTOR:  $\Delta P$  \_\_\_\_\_  $\Delta H$  \_\_\_\_\_

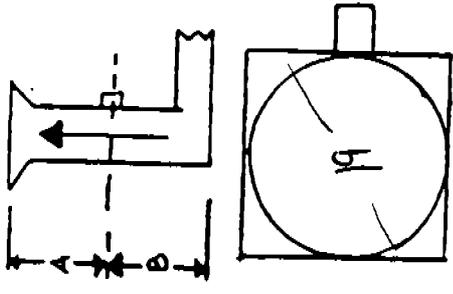


FILTER NO.: \_\_\_\_\_  
 AMBIENT TEMP.: \_\_\_\_\_  
 BARAMETRIC PRESS., IN. HG.: \_\_\_\_\_  
 ASSUMED MOISTURE: \_\_\_\_\_  
 HEATER BOX SETTING: \_\_\_\_\_  
 PROBE LENGTH, FT.: \_\_\_\_\_  
 NOZZLE DIAMETER, IN.: \_\_\_\_\_  
 PROBE HEATER SETTING: \_\_\_\_\_  
 APPROX. WIND VEL., MPH: \_\_\_\_\_  
 SAMPLE BOX TEMP., (F): \_\_\_\_\_  
 STATIC PRESSURE: \_\_\_\_\_ "H2O  
 OFFSET: \_\_\_\_\_ in. PORT DIA.: \_\_\_\_\_ in. ( M / " )

TRAVERSE POINT NUMBER	DISTANCE INCHES	O2 (%)	CO2 (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY IN. H2O		PRESSURE DIFF ORIFICE METER ( $\Delta H$ ) IN. H2O	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GAS METER		PUMP VACUUM IN. HG.	TEMP. LAST IMPINGER (F)
						$\Delta P$	$\Delta P$			INLET (Tm),	OUTLET (Tm)		
1				4:25	0	147	.285	1.21	467.6	74	74		
2				3			.295	1.36	469.5	84	75		
3				6			.30	1.39	471.3	85	75		
4				9			.31	1.44	473.3	88	74		
5				12		147	.315	1.48	475.1	89	75		
6				15		148	.30	1.41	477.0	90	76		
7				18		148	.285	1.34	478.9	91	76		
8				21		148	.275	1.29	480.8	91	77		
9				24		148	.270	1.27	482.7	95	79		
10				27		147	.255	1.19	184.4	95	79		
11				30		148	.255	1.19	486.2	95	78		
12				36		148	.255	1.19	487.9	96	78		
AVERAGE				72		146.9	0.536	1.350	482.250	87.0			

PITOT LEAK CHECK:  
 BEFORE: TOP  $\Delta P$  = \_\_\_\_\_ BOTTOM  $\Delta P$  = \_\_\_\_\_  
 AFTER: TOP  $\Delta P$  = \_\_\_\_\_ BOTTOM  $\Delta P$  = \_\_\_\_\_  
 SAMPLE TRAIN LEAK:  
 BEFORE: CFM@ \_\_\_\_\_ IN. HG.  
 AFTER: CFM@ \_\_\_\_\_ IN. HG.  
 COMMENTS: \_\_\_\_\_ PURGE \_\_\_\_\_

PLANT: Courtesy Line Gun  
 LOCATION: Hanford  
 COUNTY: Kings  
 UNIT: Motel  
 DATE: 12/4/90  
 RUN NO/METHOD: 1A-~~PM16~~  
 COLD BOX NO.: 4  
 METER BOX NO.: D  
 METER FACTOR: 9685 ΔH = 2.1055  
 PITOT #/FACTOR: #7-0.850  
 PYROMETER #: 7.5  
 MAGNEHELIC FACTOR: ΔP 1.008 ΔH

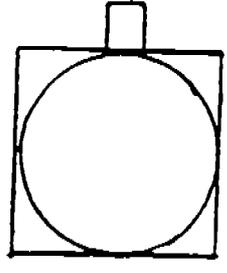
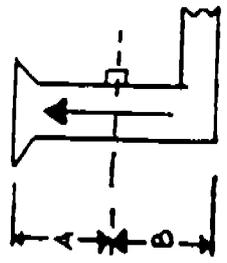


FILTER NO. \_\_\_\_\_  
 AMBIENT TEMP.: 44 F  
 BAROMETRIC PRESS., IN. HG.: 30.21  
 ASSUMED MOISTURE: 5%  
 HEATER BOX SETTING: \_\_\_\_\_  
 PROBE LENGTH, FT.: 5  
 NOZZLE DIAMETER, IN.: .211  
 PROBE HEATER SETTING: \_\_\_\_\_  
 APPROX. WIND VEL., MPH: calm  
 SAMPLE BOX TEMP., (F): \_\_\_\_\_  
 STATIC PRESSURE: -0.15 "H2O  
 OFFSET: 0 in. PORT DIA.: 3 in. ( M / )

TRAVERSE POINT NUMBER	DISTANCE INCHES	O2 (%)	CO2 (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY IN. H2O		PRESSURE DIFF ORIFICE METER (ΔH) IN. H2O	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GAS METER		PUMP VACUUM IN. HG.	TEMP. LAST IMPINGER (F)
						ΔP	ΔP			INLET (Tm),	OUTLET (Tm)		
1				9:00	55	.35		.79	520.871	43	43		
2				3	56	.40		.91	522.2	45	43		
3				6	56	.40		.92	523.6	51	46		
4				9	56	.42		.96	525.1	55	46		
5				12	58	.43		.99	526.6	57	46		
6				15	59	.45		1.04	528.2	62	50		
7				18	59	.55		1.26	529.8	65	50		
8				21	60	.60		1.38	531.6	66	50		
9				24	60	.60		1.38	533.3	67	51		
10				27	60	.67		1.55	535.1	69	54		
11				30	61	.65		1.51	537.1	70	55		
12				33	61	.72		1.67	539.0	75	60	13	
				36					540.9				
AVERAGE													

PITOT LEAK CHECK: BEFORE: TOP ΔP = \_\_\_\_\_ ΔP = \_\_\_\_\_ BOTTOM ΔP = \_\_\_\_\_  
 AFTER: TOP ΔP = \_\_\_\_\_ ΔP = \_\_\_\_\_ BOTTOM ΔP = \_\_\_\_\_  
 SAMPLE TRAIN LEAK: BEFORE = 2.005 CRM @ \_\_\_\_\_ IN. HG.  
 AFTER = 2.005 CRM @ \_\_\_\_\_ IN. HG.  
 COMMENTS: \_\_\_\_\_ PURGE \_\_\_\_\_

PLANT: County Line Gin  
 LOCATION: \_\_\_\_\_  
 COUNTY: \_\_\_\_\_  
 UNIT: None  
 DATE: 12/4/90  
 RUN NO./METHOD: IR-P410  
 COLD BOX NO.: 4  
 METER BOX NO.: \_\_\_\_\_  
 METER FACTOR: \_\_\_\_\_  
 PITOT #/FACTOR: \_\_\_\_\_  
 PYROMETER #: \_\_\_\_\_  
 MAGNETIC FACTOR:  $\Delta P$  \_\_\_\_\_  $\Delta H$  \_\_\_\_\_



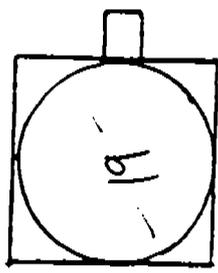
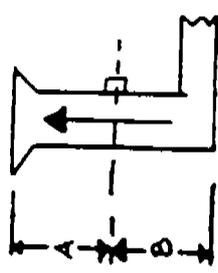
FILTER NO.: \_\_\_\_\_  
 AMBIENT TEMP.: \_\_\_\_\_  
 BAROMETRIC PRESS., IN. HG.: \_\_\_\_\_  
 ASSUMED MOISTURE: \_\_\_\_\_  
 HEATER BOX SETTING: \_\_\_\_\_  
 PROBE LENGTH, FT.: \_\_\_\_\_  
 NOZZLE DIAMETER, IN.: 2.11  
 PROBE HEATER SETTING: \_\_\_\_\_  
 APPROX. WIND VEL., MPH: \_\_\_\_\_  
 SAMPLE BOX TEMP., (F): \_\_\_\_\_  
 STATIC PRESSURE: \_\_\_\_\_ "H2O  
 OFFSET: \_\_\_\_\_ in. PORT DIA.: \_\_\_\_\_ in. ( M / )

TRAVERSE POINT NUMBER	DISTANCE INCHES	O2 (%)	CO2 (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY IN. H2O		PRESSURE DIFF ORIFICE METER ( $\Delta H$ ) IN. H2O	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GAS METER		PUMP VACUUM IN. HG.	TEMP. LAST IMPINGER (F)
						$\Delta P$	$\Delta P$			INLET (Tm),	OUTLET (Tm)		
1				9:40	61	.45		1.04	540.9	61	60		
2				3	62	.60		1.40	542.5	71	62		
3				6	64	.60		1.4	544.3	73	63		
4				9	64	.65		1.52	546.2	75	63	12	
5				12	64	.65		1.52	548.1	76	63		
6				15	64	.60		1.40	550.1	77	63		
7				18	64	.50		1.17	551.9	77	64		
8				21	64	.50		1.17	553.6	79	65		
9				24	65	.50		1.17	555.2	82	66		
10				27	65	.55		1.31	556.9	83	67		
11				30	66	.55		1.31	558.7	83	67		
12				37	66	.55		1.31	560.5	84	67		
	ZERO			36					562.211				
	SPAN												
AVERAGE		10.9	0.05	92	67		0.73	1.253	413.40		62.7		

SAMPLE TRAIN LEAK:  
 BEFORE: \_\_\_\_\_ IN. HG.  
 AFTER: \_\_\_\_\_ IN. HG.  
 COMMENTS: \_\_\_\_\_

97

PLANT: Courtesy Line Gwh  
 LOCATION: Hanford  
 COUNTY: Kings  
 UNIT: Mofo  
 DATE: 12/4/90  
 RUN NO./METHOD: 2A - PM10  
 COLD BOX NO.: 9  
 METER BOX NO.: # D  
 METER FACTOR: .9685  $\Delta H_0 = 2.1055$   
 PITOT # FACTOR: .85  
 PYROMETER #: 75  
 MAGNEHELIC FACTOR:  $\Delta P 7.008$   $\Delta H 0.152$



FILTER NO.: 65  
 AMBIENT TEMP.: 30.21  
 BAROMETRIC PRESS., IN. HG.: 59.0  
 ASSUMED MOISTURE: —  
 HEATER BOX SETTING: 81  
 PROBE LENGTH, FT.: 211  
 NOZZLE DIAMETER, IN.: —  
 PROBE HEATER SETTING: Caliber  
 APPROX. WIND VEL., MPH: —  
 SAMPLE BOX TEMP., (F): —  
 STATIC PRESSURE: — in. H<sub>2</sub>O  
 OFFSET: φ in. PORT DIA.: 3 in. (M / )

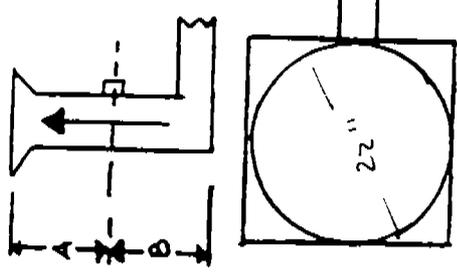
TRAVERSE POINT NUMBER	DISTANCE INCHES	O2 (%)	CO2 (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY IN. H2O		PRESSURE DIFF ORIFICE METER (ΔH) IN. H2O	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GASMETER		PUMP VACUUM IN. HG.	TEMP. LAST IMPINGER (F)
						ΔP	√ΔP			INLET (Tm),	OUTLET (Tm)		
1				10.460	70	.135		.81	562.651	64	64		
2				2.5	71	.40		.94	563.9	67	63		
3				5	72	.40		.94	565.2	69	63		
4				7.5	72	.42		.96	566.4	70	63		
5				10	72	.43		.99	567.6	76	64		
6				12.5	73	.45		1.01	569.2	83	65		
7				15	74	.55		1.27	570.5	86	65		
8				17.5	74	.60		1.40	571.9	87	65		
9				20	74	.67		1.40	573.5	89	70		
10				22.5	75	.65		1.58	575.0	89	70		
11				25	75	.70		1.52	576.7	91	73		
12				27.5	75	.70		1.63	578.3	92	73	7	
				30					579.9				
AVERAGE													

PITOT LEAK CHECK:  
 BEFORE: TOP ΔP = \_\_\_\_\_ BOTTOM ΔP = \_\_\_\_\_  
 AFTER: TOP ΔP = \_\_\_\_\_ BOTTOM ΔP = \_\_\_\_\_  
 COMMENTS: \_\_\_\_\_

SAMPLE TRAIN LEAK:  
 BEFORE = 2.002 CFM @ 15 IN. HG.  
 AFTER = 1.005 CFM @ 15 IN. HG.



PLANT: Country Lane Gas  
 LOCATION: Hanford  
 COUNTY: Kings  
 UNIT: West Trap  
 DATE: 12/4/90  
 RUN NO./METHOD: 1A - PM 10  
 COLD BOX NO.: 4  
 METER BOX NO.: D  
 METER FACTOR: .9605  $\Delta H_0 = 2.1055$   
 PITOT #/FACTOR: 47 - 0.550  
 PYROMETER #: 1-3  
 MAGNEHELIC FACTOR:  $\Delta P$  1.008  $\Delta H$  0.952

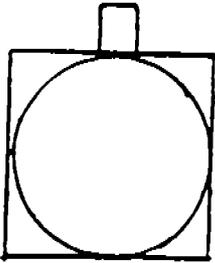
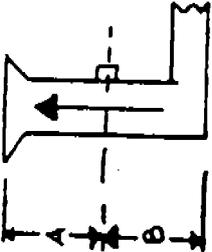


FILTER NO. \_\_\_\_\_  
 AMBIENT TEMP.: 75  
 BARAMETRIC PRESS., IN. HG.: 30.1  
 ASSUMED MOISTURE: 5%  
 HEATER BOX SETTING: \_\_\_\_\_  
 PROBE LENGTH, FT.: 5'  
 NOZZLE DIAMETER, IN.: .211  
 PROBE HEATER SETTING: \_\_\_\_\_  
 APPROX. WIND VEL., MPH: calm  
 SAMPLE BOX TEMP., (F): \_\_\_\_\_  
 STATIC PRESSURE: 0.10 "H2O  
 OFFSET: \_\_\_\_\_ in. PORT DIA.: \_\_\_\_\_ in. ( M / )

TRAVERSE POINT NUMBER	DISTANCE INCHES	O2 (%)	CO2 (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY IN. H2O		PRESSURE DIFF ORIFICE METER (ΔH) IN. H2O	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GASMETER		PUMP VACUUM IN. HG.	TEMP. LAST IMPINGER (F)
						ΔP	√ΔP			INLET (Tm),	OUTLET (TM)		
1				1:11	98	.25		.55	598.121	66	66		
2				3	99	.28		.62	599.3	71	66		
3				6	97	.30		.67	600.5	71	66		
4				9	98	.30		.67	601.7	78	68		
5				12	99	.29		.65	603.1	78	68		
6				15	100	.29		.65	604.2	81	69		
7				18	100	.30		.67	605.5	86	71		
8				21	101	.32		.71	606.8	87	72		
9				24	102	.37		.83	608.2	90	74		
10				27	102	.42		.95	609.6	91	75		
11				30	100	.42		.97	611.2	92	76		
12				33	103	.45		1.02	612.7	94	77		
				36					614.2				
AVERAGE													
PTOT LEAK CHECK:													
BEFORE: TOP ΔP= _____ BOTTOM ΔP= _____													
AFTER: TOP ΔP= _____ BOTTOM ΔP= _____													
SAMPLE TRAIN LEAK: CRM@ _____ IN. HG.													
AFTER: CRM@ _____ IN. HG.													
COMMENTS: _____ PURGE _____													

201

PLANT: \_\_\_\_\_  
 LOCATION: \_\_\_\_\_  
 COUNTY: \_\_\_\_\_  
 UNIT: Unit Prep  
 DATE: 12/9/90  
 RUN NO./METHOD: 1B - PM10  
 COLD BOX NO.: \_\_\_\_\_  
 METER BOX NO.: \_\_\_\_\_  
 METER FACTOR: \_\_\_\_\_  
 PITOT #/FACTOR: \_\_\_\_\_  
 PYROMETER #: \_\_\_\_\_  
 MAGNETIC FACTOR:  $\Delta P$  \_\_\_\_\_  $\Delta H$  \_\_\_\_\_



FILTER NO.: \_\_\_\_\_  
 AMBIENT TEMP.: \_\_\_\_\_  
 BAROMETRIC PRESS., IN. HG.: \_\_\_\_\_  
 ASSUMED MOISTURE: \_\_\_\_\_  
 HEATER BOX SETTING: \_\_\_\_\_  
 PROBE LENGTH, FT.: \_\_\_\_\_  
 NOZZLE DIAMETER, IN.: .211  
 PROBE HEATER SETTING: \_\_\_\_\_  
 APPROX. WIND VEL., MPH: \_\_\_\_\_  
 SAMPLE BOX TEMP., (F): \_\_\_\_\_  
 STATIC PRESSURE: \_\_\_\_\_ "H2O  
 OFFSET: \_\_\_\_\_ in. PORT DIA.: \_\_\_\_\_ in. ( M / )

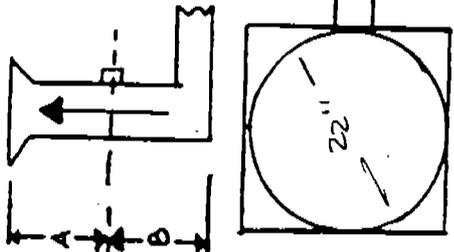
TRAVERSE POINT NUMBER	DISTANCE INCHES	O2 (%)	CO2 (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY HEAD IN. H2O		PRESSURE DIFF ORIFICE METER ( $\Delta H$ ) IN. H2O	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GAS METER		PUMP VACUUM IN. HG.	TEMP. LAST IMPINGER (F)
						$\Delta P$	$\sqrt{\Delta P}$			INLET (Tm),	OUTLET (Tm)		
1				0	110	.41		.90	614.2	79	79		
2				3	110	.42		.93	615.7	80	78		
3				6	111	.45		1.0	617.3	89	78		
4				9	111	.45		1.0	618.8	91	78		
5				12	111	.41		.91	610.4	91	79		
6				15	111	.30		.66	614.9	91	80		
7				18	112	.30		.66	622.1	91	80		
8				21	112	.32		.71	622.2	91	80		
9				24	112	.39		.82	624.7	95	81		
10				27	112	.42		.73	626.0	96	82		
11				30	111	.42		.93	627.5	96	82		
12				33	110	.40		.90	629.1	97	82		
12	ZERO SPAN			36					630.540				
AVERAGE		20.9	0.05	72	105.5		0.548	0.801	32.419	81.1			

PITOT LEAK CHECK:  
 BEFORE: TOP  $\Delta P$  = \_\_\_\_\_ BOTTOM  $\Delta P$  = \_\_\_\_\_  
 AFTER: TOP  $\Delta P$  = \_\_\_\_\_ BOTTOM  $\Delta P$  = \_\_\_\_\_

SAMPLE TRAIN LEAK:  
 BEFORE CRM@ \_\_\_\_\_ IN. HG.  
 AFTER CRM@ \_\_\_\_\_ IN. HG.

COMMENTS: \_\_\_\_\_ PURGE \_\_\_\_\_

PLANT: Country Line Gas  
 LOCATION: Hanford  
 COUNTY: Kings  
 UNIT: First U-Trap  
 DATE: 12/4/90  
 RUN NO./METHOD: 2A - PULP  
 COLD BOX NO.: 9  
 METER BOX NO.: D  
 METER FACTOR: 9685 AHG = 2.1055  
 PITOT #/FACTOR: 17-0.850  
 PYROMETER #: 176  
 MAGNEHELIC FACTOR:  $\Delta P$  1.008  $\Delta H$  0.952



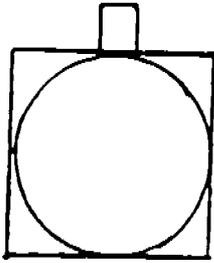
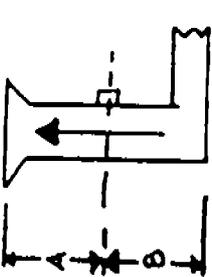
FILTER NO.: \_\_\_\_\_  
 AMBIENT TEMP.: 75  
 BAROMETRIC PRESS., IN. HG.: 30.1  
 ASSUMED MOISTURE: 5.9%  
 HEATER BOX SETTING: \_\_\_\_\_  
 PROBE LENGTH, FT.: 5'  
 NOZZLE DIAMETER, IN.: 2.11  
 PROBE HEATER SETTING: \_\_\_\_\_  
 APPROX. WIND VEL., MPH: calm  
 SAMPLE BOX TEMP., (F): \_\_\_\_\_  
 STATIC PRESSURE: -.10 "H<sub>2</sub>O  
 OFFSET: 0 in. PORT DIA.: 3 in. (M / -)

TRAVERSE POINT NUMBER	DISTANCE INCHES	O <sub>2</sub> (%)	CO <sub>2</sub> (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY IN. H <sub>2</sub> O		PRESSURE DIFF ORIFICE METER ( $\Delta H$ ) IN. H <sub>2</sub> O	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GAS METER		PUMP VACUUM IN. HG.	TEMP. LAST IMPINGER (F)
						$\Delta P$	$\sqrt{\Delta P}$			INLET (Tm),	OUTLET (Tm)		
1				2:58	110	.25		.54	630.652	74	74		
2				3	110	.28		.61	631.8	78	71		
3				6	110	.3		.66	633.0	80	71		
4				9	111	.3		.66	634.2	83	75		
5				12	111	.3		.66	635.5	84	73		
6				15	111	.28		.62	636.7	87	75		
7				18	110	.29		.64	638.0	90	80.75		
8				21	109	.25		.71	639.2	90	75		
9				24	109	.37		.81	640.6	72	72		
10				27	109	.4		.88	642.1	79	73		
11	Gas Sample Temp. Behind B-42			30	109	.42	0.5	.92	643.5	83	73		
12				33	96	.45		.99	645.1	86	73		
	ZERO SPAN			36					646.5				
AVERAGE													

PITOT LEAK CHECK:  
 BEFORE: \_\_\_\_\_  
 AFTER: \_\_\_\_\_  
 TOP  $\Delta P$  = \_\_\_\_\_  
 $\Delta P$  = \_\_\_\_\_  
 BOTTOM  $\Delta P$  = \_\_\_\_\_  
 $\Delta P$  = \_\_\_\_\_  
 COMMENTS: \_\_\_\_\_  
 PURGE \_\_\_\_\_

SAMPLE TRAIN LEAK:  
 BEFORE: 4.005 IN. HG.  
 AFTER: 4.005 IN. HG.  
 CFM@ \_\_\_\_\_  
 CFM@ \_\_\_\_\_

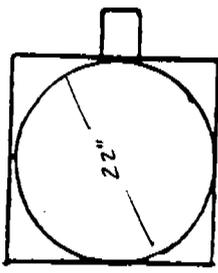
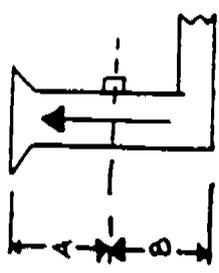
PLANT: \_\_\_\_\_  
 LOCATION: \_\_\_\_\_  
 COUNTY: \_\_\_\_\_  
 UNIT: Lint Trap  
 DATE: 12/4/50  
 RUN NO./METHOD: 2B - PM10  
 COLD BOX NO.: \_\_\_\_\_  
 METER BOX NO.: \_\_\_\_\_  
 METER FACTOR: \_\_\_\_\_  
 PITOT #/FACTOR: \_\_\_\_\_  
 PYROMETER #: \_\_\_\_\_  
 MAGNEHELIC FACTOR:  $\Delta P$  \_\_\_\_\_  $\Delta H$  \_\_\_\_\_



FILTER NO. \_\_\_\_\_  
 AMBIENT TEMP.: \_\_\_\_\_  
 BAROMETRIC PRESS., IN. HG.: \_\_\_\_\_  
 ASSUMED MOISTURE: \_\_\_\_\_  
 HEATER BOX SETTING: \_\_\_\_\_  
 PROBE LENGTH, FT.: 2.11  
 NOZZLE DIAMETER, IN.: \_\_\_\_\_  
 PROBE HEATER SETTING: \_\_\_\_\_  
 APPROX. WIND VEL., MPH: \_\_\_\_\_  
 SAMPLE BOX TEMP., (F): \_\_\_\_\_  
 STATIC PRESSURE: \_\_\_\_\_  
 OFFSET: \_\_\_\_\_ in. PORT DIA.: \_\_\_\_\_ in. ( M / )

TRAVERSE POINT NUMBER	DISTANCE INCHES	O2 (%)	CO2 (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY IN. H2O		PRESSURE DIFF ORIFICE METER (ΔH) IN. H2O	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GAS METER		PUMP VACUUM IN. HG.	TEMP. LAST IMPINGER (F)
						ΔP	√ΔP			INLET (Tm),	OUTLET (Tm)		
1				3:59	96	.40		.89	646.5	73	73		
2				7	97	.43		.96	648.0	80	73		
3				6	97	.43		.96	649.6	86	74		
4				9	98	.45		1.01	651.1	86	74		
5				12	98	.45		1.01	652.9	90	75		
6				15	99	.45		1.01	654.3	91	75		
7				18	99	.46		.91	655.9	92	77		
8				21	100	.30		.68	657.4	93	78		
9				24	98	.30		.68	658.6	92	78		
10				27	93	.35		.79	659.9	94	78		
11				30	94	.42		.95	661.3	94	79		
12				33	94	.46		.91	662.8	95	80		
				36					664.376				
AVERAGE			20.91005	77	102.8			0.813	99.678	80.7			
PITOT LEAK CHECK:													
BEFORE: TOP ΔP= _____ BOTTOM ΔP= _____													
AFTER: TOP ΔP= _____ BOTTOM ΔP= _____													
SAMPLE TRAIN LEAK: CRM@ _____ IN. HG.													
CRM@ _____ IN. HG.													
COMMENTS: _____ PURGE _____													

PLANT: County Line Gin  
 LOCATION: Hanford  
 COUNTY: Kings  
 UNIT: Station  
 DATE: 12/3/90  
 RUN NO./METHOD: 1A ~ PM 10  
 COLD BOX NO.: 484  
 METER BOX NO.: E  
 METER FACTOR: 1.0231  
 PITOT #/FACTOR: 47 - 0.850  
 PYROMETER #:  
 MAGNEHELIC FACTOR:  $\Delta P$  1.005  $\Delta H$  0.995

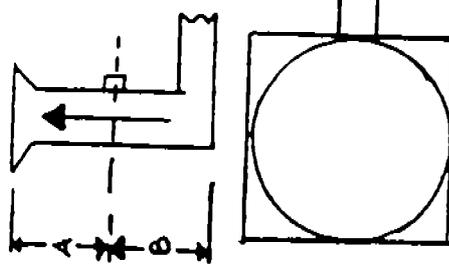


FILTER NO.:  
 AMBIENT TEMP.: 40F  
 BARAMETRIC PRESS., IN. HG.: 30.27  
 ASSUMED MOISTURE: 5%  
 HEATER BOX SETTING:  
 PROBE LENGTH, FT.: 5  
 NOZZLE DIAMETER, IN.: .296  
 PROBE HEATER SETTING:  
 APPROX. WIND VEL., MPH:  
 SAMPLE BOX TEMP., (F):  
 STATIC PRESSURE: -0.03 "H2O  
 OFFSET: 0 in. PORT DIA.: 3 in. (M / )

TRAVERSE POINT NUMBER	DISTANCE INCHES	O2 (%)	CO2 (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY IN. H2O		PRESSURE DIFF ORIFICE METER (ΔH) IN. H2O	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GAS METER		PUMP VACUUM IN. HG.	TEMP. LAST IMPINGER (F)		
						ΔP	√ΔP			INLET (Tm),	OUTLET (Tm)				
1				1.31	72	.115		.98	279.7	50	50				
2				3	73	.140		1.19	281.3	51	50	7			
3				6	73	.150		1.28	283.1	56	50				
4				9	74	.165		1.42	284.7	62	51				
5				12	74	.165		1.42	286.5	66	51				
6				15	74	.180		1.57	288.3	69	55				
7				18	74	.180		1.57	290.4	71	55	9			
8				21	74	.185		1.62	292.1	73	57				
9				24	74	.162		1.44	294	75	58				
10				27	75	.155		1.38	295.9	77	60				
11				30	75	.145		1.29	297.7	77	60				
12				33	75	.140		1.24	299.4	78	63				
AVERAGE				36	74				301.1						
PTOT LEAK CHECK:															
BEFORE:						TOP ΔP =			BOTTOM ΔP =			BEFORE =		SAMPLE TRAIN LEAK:	
AFTER:						TOP ΔP =			BOTTOM ΔP =			AFTER =		CRM@ 15 IN. HG.	
						TOP ΔP =			BOTTOM ΔP =					CRM@ IN. HG.	
						TOP ΔP =			BOTTOM ΔP =					PURGE	
COMMENTS:															

Ball # 32760 104

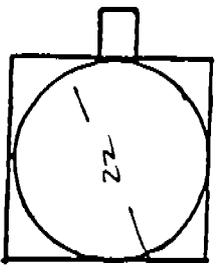
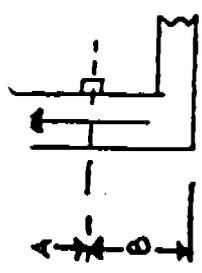
PLANT: Country Lane Gas  
 LOCATION: \_\_\_\_\_  
 COUNTY: \_\_\_\_\_  
 UNIT: Sychar  
 DATE: 12/3/90  
 RUN NO./METHOD: 1B ~ PM 10  
 COLD BOX NO.: 4  
 METER BOX NO.: \_\_\_\_\_  
 METER FACTOR: \_\_\_\_\_  
 PITOT #/FACTOR: \_\_\_\_\_  
 PYROMETER #: \_\_\_\_\_  
 MAGNETIC FACTOR:  $\Delta P$  \_\_\_\_\_  $\Delta H$  \_\_\_\_\_



FILTER NO.: \_\_\_\_\_  
 AMBIENT TEMP.: \_\_\_\_\_  
 BAROMETRIC PRESS., IN. HG.: \_\_\_\_\_  
 ASSUMED MOISTURE: \_\_\_\_\_  
 HEATER BOX SETTING: \_\_\_\_\_  
 PROBE LENGTH, FT.: \_\_\_\_\_  
 NOZZLE DIAMETER, IN.: \_\_\_\_\_  
 PROBE HEATER SETTING: \_\_\_\_\_  
 APPROX. WIND VEL., MPH: \_\_\_\_\_  
 SAMPLE BOX TEMP., (F): \_\_\_\_\_  
 STATIC PRESSURE: \_\_\_\_\_ "H<sub>2</sub>O  
 OFFSET: \_\_\_\_\_ in. PORT DIA.: \_\_\_\_\_ in. ( M / )

TRAVERSE POINT NUMBER	DISTANCE INCHES	O <sub>2</sub> (%)	CO <sub>2</sub> (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY IN. H <sub>2</sub> O		PRESSURE DIFF ORIFICE METER (ΔH) IN. H <sub>2</sub> O	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GASMETER (Tm),		PUMP VACUUM IN. HG.	TEMP. LAST IMPINGER (F)
						ΔP	√ΔP			INLET	OUTLET		
1				10:06	77	.12		1.04	301.1	65	65	7	
2				3		.12		1.05	302.7	75	66		
3				6		.115		1.02	304.4	77	68		
4				9		.135		1.20	305.9	77	69		
5				12		.155		1.37	307.6	80	70		
6				15		.185		1.73	309.4	81	70		
7				18		.21		1.85	311.3	81	69		
8				21		.21		1.86	313.3	82	70		
9				24		.21		1.86	315.5	82	69		
10				27		.2		1.78	317.6	83	71		
11				30		.185		1.64	319.6	83	70		
12				33		.175		1.56	321.6	84	72		
13				36					323.540				
AVERAGE		20.9	0.05	77	75.5		0.102	1.432	43.776		67.6		
PTOT LEAK CHECK:													
BEFORE: TOP ΔP= _____ BOTTOM ΔP= _____													
AFTER: TOP ΔP= _____ BOTTOM ΔP= _____													
SAMPLE TRAIN LEAK: CRM@ _____ IN. HG.													
CRM@ _____ IN. HG.													
COMMENTS: _____ PURGE _____													

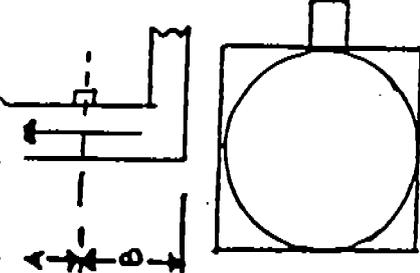
LOCATION: Haystack  
 COUNTY: Kings  
 UNIT: Suction  
 DATE: 12/3/90  
 RUN NO. METHOD: 2A ~ PM 10  
 COLD BOX NO.: 9  
 METER BOX NO.: E  
 METER FACTOR: 1.0231  $\Delta H_{20} = 2.1201$   
 PITOT #/ FACTOR: 17 - 0.850  
 PYROMETER #: 5-3  
 MAGNEHELIC FACTOR:  $\Delta P$  1.005  $\Delta H$  995



FILTER NO. \_\_\_\_\_  
 AMBIENT TEMP.: 52  
 BAROMETRIC PRESS., IN. HG.: 30.27  
 ASSUMED MOISTURE: 59  
 HEATER BOX SETTING: \_\_\_\_\_  
 PROBE LENGTH, FT.: 5  
 NOZZLE DIAMETER, IN.: 2.96  
 PROBE HEATER SETTING: \_\_\_\_\_  
 APPROX. WIND VEL., MPH: \_\_\_\_\_  
 SAMPLE BOX TEMP., (F): \_\_\_\_\_  
 STATIC PRESSURE: -0.03 "H<sub>2</sub>O  
 OFFSET: \_\_\_\_\_ in. PORT DIA.: \_\_\_\_\_ in. (M / F)

TRAVERSE POINT NUMBER	DISTANCE INCHES	O2 (%)	CO2 (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY IN. H2O		PRESSURE DIFF. ORIFICE METER (ΔH) IN. H2O	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GASMETER		PUMP VACUUM IN. HG.	TEA LAST IMPINGER (F)
						ΔP	√ΔP			INLET (Tm),	OUTLET (Tm)		
1				11:45	0			1.03	323.541	63	63		
2				25	83			1.07	324.9	65	63		
3				5	84			.95	326.2	71	63		
4				2.5	85			1.16	322.5	73	65	4	
5				10	85			1.46	329.0	75	63		
6				12.5	85			1.74	330.7	78	64	6	
7				15	85			1.73	332.0	77	64		
8				17.5	85			1.78	333.7	82	65		
9				20	85			1.83	335.5	83	65		
10				22.5	85			1.83	337.1	83	67		
11				25	85			1.66	338.9	85	68		
12				27.5	85			1.44	340.5	85	69		
				30					342.0				
AVERAGE													
PITOT LEAK CHECK:													
BEFORE: TOP ΔP = _____ BOTTOM ΔP = _____													
AFTER: TOP ΔP = _____ BOTTOM ΔP = _____													
SAMPLE TRAIN LEAK: CRM@ _____ IN. HG.													
CRM@ _____ IN. HG.													
COMMENTS: _____													
PURGE _____													

LOCATION: \_\_\_\_\_  
 COUNTY: \_\_\_\_\_  
 UNIT: Subher  
 DATE: 12/3/90  
 RUN NO/METHOD: 2B - PM 10  
 COLD BOX NO.: 9  
 METER BOX NO.: \_\_\_\_\_  
 METER FACTOR: \_\_\_\_\_  
 PITOT #/ FACTOR: \_\_\_\_\_  
 PYROMETER #: \_\_\_\_\_  
 MAGNEHELIC FACTOR:  $\Delta P$  \_\_\_\_\_  $\Delta H$  \_\_\_\_\_



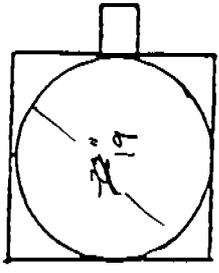
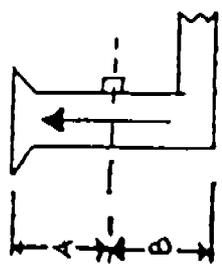
FILTER NO.: \_\_\_\_\_  
 AMBIENT TEMP.: \_\_\_\_\_  
 BAROMETRIC PRESS., IN. HG.: \_\_\_\_\_  
 ASSUMED MOISTURE: \_\_\_\_\_  
 HEATER BOX SETTING: \_\_\_\_\_  
 PROBE LENGTH, FT.: \_\_\_\_\_  
 NOZZLE DIAMETER, IN.: \_\_\_\_\_  
 PROBE HEATER SETTING: \_\_\_\_\_  
 APPROX. WIND VEL., MPH: \_\_\_\_\_  
 SAMPLE BOX TEMP., (F): \_\_\_\_\_  
 STATIC PRESSURE: \_\_\_\_\_ \*H2O  
 OFFSET: \_\_\_\_\_ in. PORT DIA.: \_\_\_\_\_ in. (M / F)

TRAVERSE POINT NUMBER	DISTANCE INCHES	O2 (%)	CO2 (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY IN. H2O		PRESSURE DIFF. ORIFICE METER ( $\Delta H$ ) IN. H2O	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GAS METER		PUMP VACUUM IN. HG.	TEA LAST IMPINGER (F)
						$\Delta P$	$\Delta P$			INLET (Tm),	OUTLET (Tm)		
1				11.45	85	.115		.997	342.0	72	72		
2				2.5	85	.130		1.13	343.3	72	72		
3				5	85	.155		1.35	344.7	70	70		
4	Bail 3200E			7.5	85	.170	0.1	1.49	346.3	70	70		
5				10	80	.175		1.51	348.1	64	64	5	
6				12.5	84	.18		1.55	349.7	70	63		
7				15	84	.18		1.55	351.2	73	64		
8				17.5	84	.19		1.64	352.8	73	63		
9				20	84	.165		1.42	354.3	78	65		
10				22.5	84	.155		1.34	356.1	80	65		
11				25	85	.145		1.26	357.5	81	66		
12				27.5	85	.145		1.26	358.8	82	66		
	ZERO			30					360.247				
	SPAN												
AVERAGE		20.9	0.05	60	84.4		0.161	1.119	361.708	71.7			

PITOT LEAK CHECK: BEFORE: TOP  $\Delta P$  = \_\_\_\_\_ BOTTOM  $\Delta P$  = \_\_\_\_\_  
 AFTER: TOP  $\Delta P$  = \_\_\_\_\_ BOTTOM  $\Delta P$  = \_\_\_\_\_  
 SAMPLE TRAIN LEAK: BEFORE: \_\_\_\_\_ IN. HG. AFTER: \_\_\_\_\_ IN. HG.  
 COMMENTS: \_\_\_\_\_ PURGE \_\_\_\_\_

201

PLANT: Country Line Gin  
 LOCATION: Hanford  
 COUNTY: Kings  
 UNIT: #1 Dwyer  
 DATE: 12/3/96  
 RUN NO/METHOD: 1A ~ P101  
 COLD BOX NO.: 4  
 METER BOX NO.: E  
 METER FACTOR: 1.0231  $\Delta H = 2.1201$   
 PITOT #/FACTOR: 11-0.850  
 PYROMETER #: \_\_\_\_\_  
 MAGNEHEUC FACTOR:  $\Delta P$  1.005  $\Delta H$  0.995



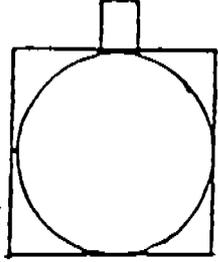
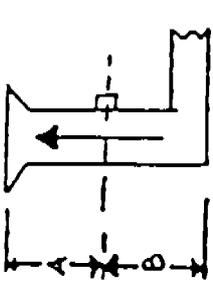
FILTER NO. \_\_\_\_\_  
 AMBIENT TEMP.: 65  
 BARAMETRIC PRESS., IN. HG.: 30.25  
 ASSUMED MOISTURE: 5%  
 HEATER BOX SETTING: \_\_\_\_\_  
 PROBE LENGTH, FT.: 5%  
 NOZZLE DIAMETER, IN.: 1.263  
 PROBE HEATER SETTING: \_\_\_\_\_  
 APPROX. WIND VEL., MPH: calm  
 SAMPLE BOX TEMP., (F): \_\_\_\_\_  
 STATIC PRESSURE: -.06 "H2O  
 OFFSET: 0 in. PORT DIA.: 3 in. (M / F)

TRAVERSE POINT NUMBER	DISTANCE INCHES	O2 (%)	CO2 (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY IN. H2O		PRESSURE DIFF. ORIFICE METER (ΔH) IN. H2O	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GAS METER		PUMP VACUUM IN. HG	TEMP. LAST IMPINGER (F)
						ΔP	√ΔP			INLET (Tm),	OUTLET (Tm)		
1				1:56	0	114	.285	1.34	360.822	61	61	9	
2					3	116	.295	1.39	362.00	67	61		
3					6	117	.295	1.40	364.0	71	62		
4					9	122	.310	1.46	365.5	73	62		
5					12	124	.315	1.5	367.6	76	64		
6					15	126	.315	1.49	369.5	78	64		
7					18	130	.305	1.46	371.4	81	67	10	
8					21	130	.28	1.32	373.4	81	68		
9					24	132	.275	1.29	375.0	82	69		
10					21	136	.27	1.26	376.9	85	72		
11					20	137	.26	1.21	378.6	86	72		
12					32	137	.255	1.19	380.2	87	73		
12					36				381.9				
AVERAGE													

PITOT LEAK CHECK:  
 BEFORE: TOP ΔP = 3.7 BOTTOM ΔP = 3.4  
 ΔP = 3.7 ΔP = 3.4  
 AFTER: TOP ΔP = 3.2 BOTTOM ΔP = 3.7  
 ΔP = 3.2 ΔP = 3.7

SAMPLE TRAIN LEAK:  
 BEFORE: CRM@ 15 IN. HG.  
 AFTER: CRM@ 15 IN. HG.  
 COMMENTS: \_\_\_\_\_  
 PURGE \_\_\_\_\_

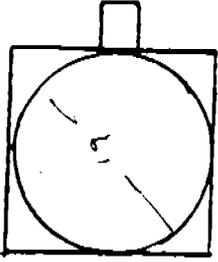
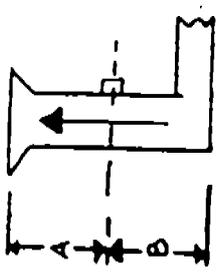
LOCATION: Courty Line Gas  
 COUNTY: Hamilton  
 UNIT: Kings  
 DATE: 12/3/90  
 RUN NO/METHOD: 2B - PM70  
 COLD BOX NO.: \_\_\_\_\_  
 METER BOX NO.: \_\_\_\_\_  
 METER FACTOR: \_\_\_\_\_  
 PITOT #/FACTOR: \_\_\_\_\_  
 PYROMETER #: \_\_\_\_\_  
 MAGNETIC FACTOR:  $\Delta P$   $\Delta H$



FILTER NO.: \_\_\_\_\_  
 AMBIENT TEMP.: \_\_\_\_\_  
 BARAMETRIC PRESS., IN. HG.: \_\_\_\_\_  
 ASSUMED MOISTURE: \_\_\_\_\_  
 HEATER BOX SETTING: \_\_\_\_\_  
 PROBE LENGTH, FT.: \_\_\_\_\_  
 NOZZLE DIAMETER, IN.: \_\_\_\_\_  
 PROBE HEATER SETTING: \_\_\_\_\_  
 APPROX. WIND VEL., MPH: \_\_\_\_\_  
 SAMPLE BOX TEMP., (F): \_\_\_\_\_  
 STATIC PRESSURE: \_\_\_\_\_ \*H2O  
 OFFSET: \_\_\_\_\_ in. PORT DIA.: \_\_\_\_\_ in. (M / F)

TRAVERSE POINT NUMBER	DISTANCE INCHES	O2 (%)	CO2 (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY IN. H2O		PRESSURE DIFF ORIFICE METER (ΔH) IN. H2O	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GAS METER		PUMP VACUUM IN. HG.	TEMP. LAST IMPINGER (F)
						ΔP	√ΔP			INLET (Tm),	OUTLET (Tm)		
1				2:34	140	.27		1.25	381.9	76	75		
2				3	142	.275		1.28	383.7	85	75		
3				4	142	.28		1.30	385.3	84	75		
4				9	141	.28		1.30	387.2	88	76	9	
5				12	140	.27		1.27	388.9	89	76		
6				15	131	.285		1.34	390.7	90	79		
7				18	135	.3		1.41	392.5	91	77		
8				21	140	.31		1.45	394.4	90	77		
9				24	139	.31		1.45	396.2	90	80		
10				27	143	.3		1.41	398.1	90	80		
11				30	130	.29		1.36	399.9	90	82		
12				33	125	.28		1.31	401.7	91	83		
36				36					403.475				
AVERAGE			20.9	0.05	72			1.352	43.153	77.3			
PITOT LEAK CHECK:													
BEFORE: TOP ΔP = _____ BOTTOM ΔP = _____													
AFTER: TOP ΔP = _____ BOTTOM ΔP = _____													
SAMPLE TRAIN LEAK: _____ IN. HG.													
CRM@ _____ IN. HG.													
CRM@ _____ IN. HG.													
COMMENTS: _____ PURGE _____													

PLANT: Courtesy Lyne Air  
 LOCATION: Hanford  
 COUNTY: Curys  
 UNIT: #1 Dye  
 DATE: 12/3/98  
 RUN NO./METHOD: 2A-PM10  
 COLD BOX NO.: 9  
 METER BOX NO.: E  
 METER FACTOR: 1.0221, ΔHC = 2.1201  
 PITOT #/FACTOR: \_\_\_\_\_  
 PYROMETER #: \_\_\_\_\_  
 MAGNEHELIC FACTOR: ΔP 1.005 ΔH 0.995



FILTER NO.: \_\_\_\_\_  
 AMBIENT TEMP.: 68  
 BARAMETRIC PRESS., IN. HG.: 30.25  
 ASSUMED MOISTURE: 5%  
 HEATER BOX SETTING: \_\_\_\_\_  
 PROBE LENGTH, FT.: 5'  
 NOZZLE DIAMETER, IN.: .263  
 PROBE HEATER SETTING: \_\_\_\_\_  
 APPROX. WIND VEL., MPH: Calm  
 SAMPLE BOX TEMP., (F): \_\_\_\_\_  
 STATIC PRESSURE: -.06 "H2O  
 OFFSET: φ in. PORT DIA.: 3 in. (M / )

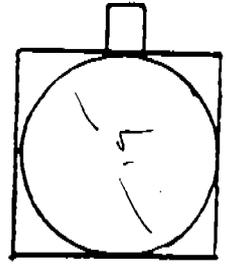
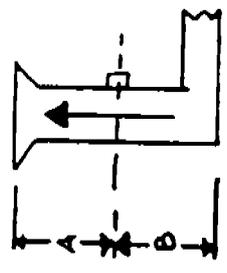
TRAVERSE POINT NUMBER	DISTANCE INCHES	O2 (%)	CO2 (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY IN. H2O		PRESSURE DIFF ORIFICE METER (ΔH) IN. H2O	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GAS METER		PUMP VACUUM IN. HG.	TEMP. LAST IMPINGER (F)
						ΔP	√ΔP			INLET (Tm),	OUTLET (Tm)		
1				0	142	.285		1.29	402.562	86	83		
2				3	146	.30		1.36	405.4	70	68		
3				6	147	.30		1.38	407.1	75	69		
4				9	147	.31		1.41	408.7	77	69		
5				12	146	.315		1.44	410.8	81	71		
6				15	148	.315		1.44	412.5	81	70		
7				18	148	.30		1.57	414.3	82	70		
8				21	148	.285		1.32	416.3	85	72		
9				24	148	.275		1.27	418.1	87	72		
10				27	148	.27		1.26	419.9	87	72		
11				30	149	.255		1.19	421.5	88	73		
12				33	150	.255		1.19	423.3	89	74		
12				36					424.9				
AVERAGE													

PITOT LEAK CHECK:  
 BEFORE: TOP ΔP = 3.2 BOTTOM ΔP = 3.5  
 ΔP = 3.12 ΔP = 3.5  
 AFTER: TOP ΔP = \_\_\_\_\_ BOTTOM ΔP = \_\_\_\_\_  
 ΔP = \_\_\_\_\_ ΔP = \_\_\_\_\_

SAMPLE TRAIN LEAK:  
 BEFORE = 1.005 CRM@ \_\_\_\_\_ IN. HG.  
 AFTER = 1.005 CRM@ \_\_\_\_\_ IN. HG.

COMMENTS: \_\_\_\_\_  
 PURGE \_\_\_\_\_

PLANT: Corrosion Line Gas  
 LOCATION: \_\_\_\_\_  
 COUNTY: \_\_\_\_\_  
 UNIT: Al Dayer  
 DATE: 12/3/96  
 RUN NO./METHOD: 28 - PM 10  
 COLD BOX NO.: \_\_\_\_\_  
 METER BOX NO.: \_\_\_\_\_  
 METER FACTOR: \_\_\_\_\_  
 PITOT #/FACTOR: \_\_\_\_\_  
 PYROMETER #: \_\_\_\_\_  
 MAGNETIC FACTOR:  $\Delta P$  \_\_\_\_\_  $\Delta H$  \_\_\_\_\_



FILTER NO.: \_\_\_\_\_  
 AMBIENT TEMP.: \_\_\_\_\_  
 BARAMETRIC PRESS., IN. HG.: \_\_\_\_\_  
 ASSUMED MOISTURE: \_\_\_\_\_  
 HEATER BOX SETTING: \_\_\_\_\_  
 PROBE LENGTH, FT.: \_\_\_\_\_  
 NOZZLE DIAMETER, IN.: \_\_\_\_\_  
 PROBE HEATER SETTING: \_\_\_\_\_  
 APPROX. WIND VEL., MPH: \_\_\_\_\_  
 SAMPLE BOX TEMP., (F): \_\_\_\_\_  
 STATIC PRESSURE: \_\_\_\_\_  
 OFFSET: \_\_\_\_\_ in.  $\Delta H$  \_\_\_\_\_ in. (M / F)

TRAVERSE POINT NUMBER	DISTANCE INCHES	O2 (%)	CO2 (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY IN. H2O		PRESSURE DIFF ORIFICE METER ( $\Delta H$ ) IN. H2O	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GAS METER		PUMP VACUUM IN. HG.	TEMP. LAST IMPINGER (F)
						$\Delta P$	$\sqrt{\Delta P}$			INLET (Tm),	OUTLET (Tm)		
1				4:26	147	<del>1.27</del>	.27	1.24	424.9	75	75		
2				3	147	<del>1.28</del>	.28	1.30	426.6	85	77		
3				6	147	<del>1.285</del>	.285	1.33	428.5	86	75		
4				9	148	1.280		1.30	430.2	86	75		
5				12	146	1.215		1.28	432.0	88	76	7	
6				15	147	1.270		1.26	433.7	87	76		
7				18	148	1.30		1.41	435.5	89	77		
8				21	148	1.31		1.43	437.3	90	76		
9				24	147	1.315		1.48	439.0	90	76		
10				27	147	1.29		1.35	440.9	90	77		
11				30	146	1.285		1.33	442.7	90	78		
12				33	148	1.285		1.33	444.5	91	78		
36				36					446.322				
AVERAGE			20.9	0.05	147.2		0.526	1.340	427.60	78.7			

PTOT LEAK CHECK:  
 BEFORE: TOP  $\Delta P$  = \_\_\_\_\_ BOTTOM  $\Delta P$  = \_\_\_\_\_  
 AFTER: TOP  $\Delta P$  = \_\_\_\_\_ BOTTOM  $\Delta P$  = \_\_\_\_\_  
 SAMPLE TRAIN LEAK:  
 BEFORE: \_\_\_\_\_ IN. HG.  
 AFTER: \_\_\_\_\_ IN. HG.  
 COMMENTS: \_\_\_\_\_ PURGE \_\_\_\_\_

**VIII. QUALITY ASSURANCE**

### DRY GAS METER CALIBRATION

Date: 10/3/90

Unit: D

Ambient Conditions

Temp: 78 F/C

Baro: 29.86 in.Hg

ORIFICE MANOMETER SETTING D,H	GASVOL WET TEST METER V,w	GASVOL DRY GAS METER Vb,	wet test tw	Temperature				Y	DH@Y
				Dry IN	Dry Out	Ave f	Time e		
				TD, IN	Tdb,	Td,	min		
0.5	5	743.814	74	78	73	79.75	13.53	0.9681	2.0535
		738.600	74	91	77				
1.0	5	749.390	74	93	80	89.75	9.88	0.9527	2.1501
		744.000	74	102	84				
1.5	5	754.906	74	105	86	96.25	7.97	0.9789	2.0742
		749.605	74	107	87				
2.0	5	760.540	74	107	87	98.25	7.03	0.9741	2.1440
		755.200	74	110	89				
								0.968	2.105

Calibration by: SALLY

Meter Factor: 0.9685

Reviewed by: \_\_\_\_\_

Delta H: 2.1055

Equations:

$$Y = (Vw \cdot Pb) \cdot (Td + 460) / Vdt - Vdb + (DelH / 13.6) \cdot (((Wt + wt) / 2) + 460)$$

$$Del H = (0.0317 \cdot Del) \cdot (((((WT + Wt) / 2) + 460) \cdot e) / Vw)^2 / ((Pb \cdot (Td + 460))$$

### DRY GAS METER CALIBRATION

Date: 10/3/90

Unit: E

Ambient Conditions

Temp: 76 F/C

Baro: 29.86 in.Hg

ORIFICE MANOMETER SETTING D,H	GASVOL WET TEST METER V,w	GASVOL DRY GAS METER Vb,	wet test tw	Temperature				Y	DH@Y
				Dry IN	Dry Out	Ave f	Time e min		
				TD, IN	Tdo,	Td,			
0.5	5	207.685	72	77	70	79.75	14.3	0.9587	2.2767
		202.400	72	94	78				
1.0	6	213.415	72	96	80	91.25	10.13	1.1669	1.5537
		208.100	72	105	84				
1.5	5	219.035	72	104	86	97.75	8.43	0.9790	2.2970
		213.700	72	112	89				
2.0	5	224.920	73	112	90	103.00	7.41	0.9879	2.3531
		219.600	73	117	93				
								1.023	2.12

Calibration by: SALLY

Meter Factor: 1.0231

Reviewed by: \_\_\_\_\_

Delta H: 2.1201

Equations:

$$Y = (V_w \cdot P_b) \cdot (T_d + 460) / (V_d \cdot T - V_{db}) + (\Delta H / 13.6) \cdot (((W_t + w_t) / 2) + 460)$$

$$\Delta H = (0.0317 \cdot \Delta e) \cdot (((((W_t + w_t) / 2) + 460) \cdot e) / V_w)^2 / ((P_b \cdot (T_d + 460))$$

## PITOT TUBE CALIBRATION

### Ambient Conditions

DATE: 9/4/90  
 UNIT NUMBER: 7

TEMPERATURE 83 F  
 RH: \_\_\_\_\_ %  
 BAROMETER: 29.96 in. hg.

Run #	Velocity fpm	ΔP (std) In. H2O	ΔP (s) in. H2O		Cp(s)	Dev	Cp(s)	Dev
			A	B	A	A	B	B
1	4005	1.00	1.42	1.41	0.831	0.002	0.834	0.001
2		1.00	1.41	1.42	0.834	0.001	0.831	0.002
3		1.00	1.41	1.41	0.834	0.001	0.834	0.001
Avg		1.00	1.41	1.41	~0.833	0.001*	~0.833	0.001*

AVERAGE: (Cp(s)A+Cp(s)B)/2 0.833

| ~Cp(s)A--Cp(s)B | = 0.000 \*

1	4478	1.25	1.64	1.65	0.864	0.001	0.864	0.001
2		1.25	1.65	1.65	0.862	0.002	0.862	0.002
3		1.25	1.64	1.65	0.864	0.001	0.864	0.001
Avg		1.25	1.64	1.65	~0.863	0.001*	~0.863	0.001*

AVERAGE: ( Cp(s)A+Cp(s)B)/2 0.863

| ~Cp(s)A--Cp(s)B | = 0.000 \*

1	4549	1.29	1.73	1.77	0.855	0.000	0.855	0.000
2		1.29	1.74	1.77	0.852	0.002	0.852	0.002
3		1.29	1.72	1.77	0.857	0.002	0.857	0.002
Avg		1.29	1.73	1.77	~0.855	0.002*	~0.855	0.002*

AVERAGE: (Cp(s)A+Cp(s)B)/2 0.855

| ~Cp(s)A--Cp(s)B | = 0.000 \*

### PITOT CALIBRATION VALUE:

~ Denotes average value

\* Denotes values which must be ≤ to 0.01 for calibration to be valid.

Calibrated by: RTR

Reviewed by: \_\_\_\_\_

0.850

**THERMO COUPLE CALIBRATION**

Date: 11/20/90

Unit: T-5

Point	* Standard Temperature <i>Tstd</i>		Pyrometer Temperature <i>Tpyr</i>		Error % ** $(Tstd - Tpyr) / Tstd$
	deg. F		deg. F		
1 Ambient	69.8		70.6		0.15%
2 Ice	32.0		32.8		0.16%
3 Boil	213.4		213.6		0.03%
4 Oil					0.00%

Std. Corr. Factor 0.988

Calibration by: RTR

\* Standard ID: LABCRAFT #227-694

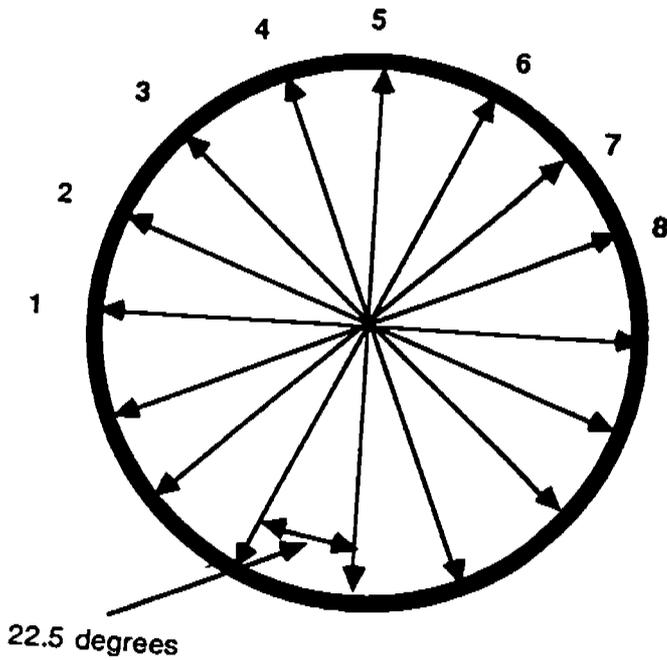
Reviewed by: \_\_\_\_\_

\* \* in deg. K

### Nozzle Calibration

Nozzle I.D. : 21

Date : 7/28/90



Points	
1 -	<u>0.212</u>
2 -	<u>0.210</u>
3 -	<u>0.211</u>
4 -	<u>0.211</u>
5 -	<u>0.210</u>
6 -	<u>0.212</u>
7 -	<u>0.211</u>
8 -	<u>0.213</u>

Average Nozzle Diameter = 0.211

Analyst : RTR

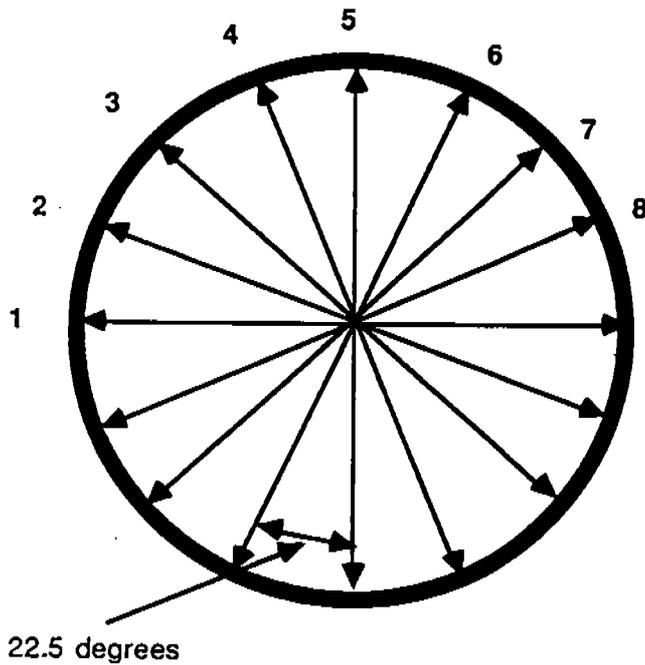
Reviewed :

117

# Nozzle Calibration

Nozzle I.D. : 22

Date : 8/24/90



Points	
1 -	<u>0.221</u>
2 -	<u>0.223</u>
3 -	<u>0.223</u>
4 -	<u>0.223</u>
5 -	<u>0.223</u>
6 -	<u>0.223</u>
7 -	<u>0.224</u>
8 -	<u>0.221</u>

Average Nozzle Diameter = 0.223

Analyst : SW

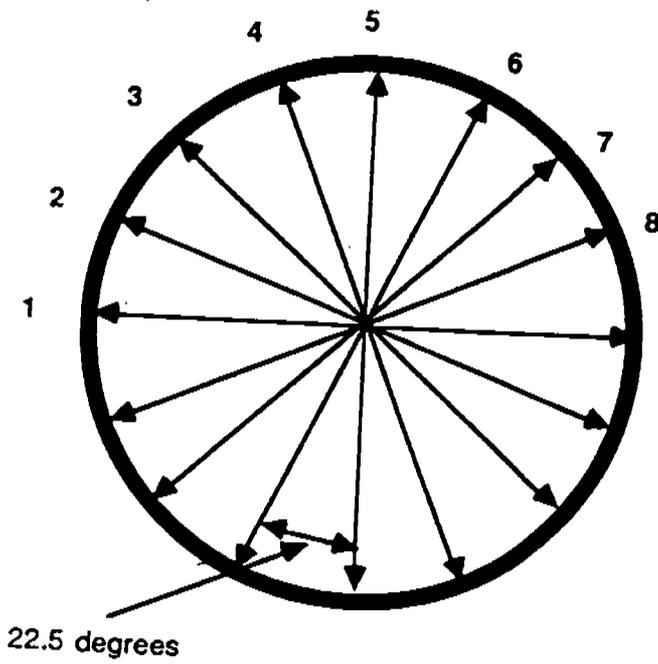
Reviewed :

BTC Environmental, Inc. - 1989

# Nozzle Calibration

Nozzle I.D. :       #25      

Date :       7/28/90      



Points	
1 -	<u>0.254</u>
2 -	<u>0.256</u>
3 -	<u>0.256</u>
4 -	<u>0.257</u>
5 -	<u>0.254</u>
6 -	<u>0.254</u>
7 -	<u>0.258</u>
8 -	<u>0.256</u>

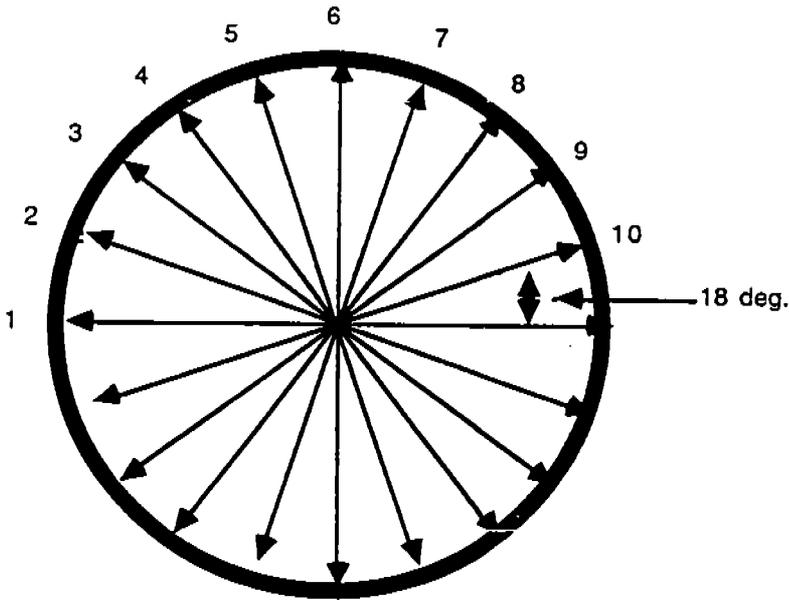
Average Nozzle Diameter =       0.255      

Analyst :    ODD   

Reviewed :    MRP

# Nozzle Calibration

Nozzle I.D. #15/25



Points	
1	0.268
2	0.270
3	0.267
4	0.267
5	0.267
6	0.265
7	0.268
8	0.265
9	0.265
10	

Average Nozzle Diameter = 0.268

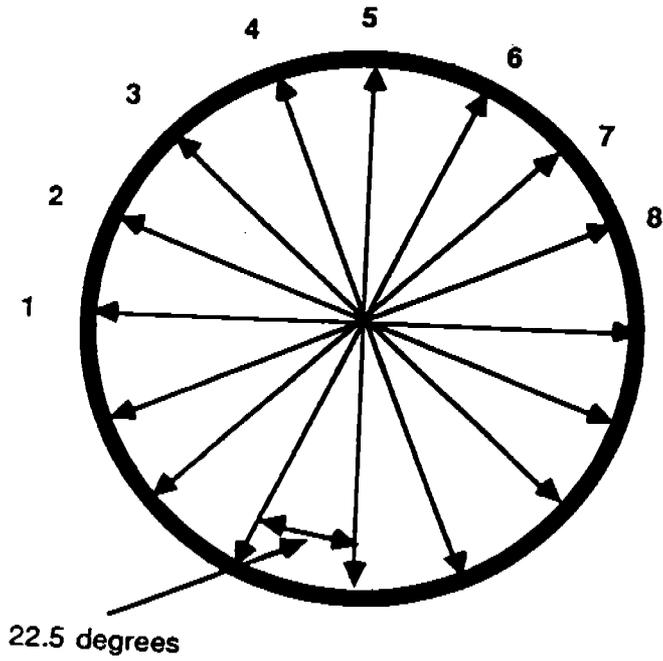
Analyst RTR

Date 6/23/89

# Nozzle Calibration

Nozzle I.D. : #33

Date : 7/28/90



Points	
1 -	<u>0.397</u>
2 -	<u>0.398</u>
3 -	<u>0.398</u>
4 -	<u>0.399</u>
5 -	<u>0.399</u>
6 -	<u>0.399</u>
7 -	<u>0.397</u>
8 -	<u>0.398</u>

Average Nozzle Diameter = 0.298

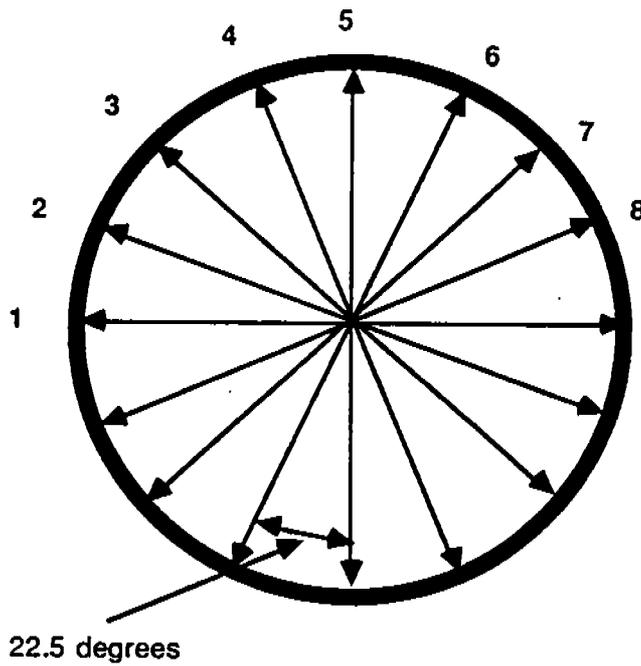
Analyst : CDD

Reviewed : MRP

# Nozzle Calibration

Nozzle I.D. :     #34    

Date :     01/08/90    



Points	
1-	<u>0.297</u>
2-	<u>0.296</u>
3-	<u>0.296</u>
4-	<u>0.294</u>
5-	<u>0.294</u>
6-	<u>0.295</u>
7-	<u>0.296</u>
8-	<u>0.296</u>

Average Nozzle Diameter = 0.296

Analyst : RTB

Reviewed :

## MAGNEHELIC CALIBRATION

DATE: 8/23/89  
 GAGE ID # M-2  
 RANGE 0-2 in. H2O

SCHEDULED CALIBRATION:  
 SEMI-ANNUAL   
 BI-MONTHLY   
 OTHER

REFERENCE ID # #424 0-10

**LEAK CHECK:**

System:	† Set @ 10 in. H2O	vacuum 10 in. P F	pressure 10 in. P F
Point:	†† Set @ 90 % FS in. H2O	vacuum in. P F	pressure in. P F

Point	Incline Delta P <i>Pinc</i>	Magnehelic Delta P <i>Pmag</i>	% Deviation $(Pinc - Pmag) / Pinc \times 100$
1	0.400	0.41	2.500%
	0.400	0.41	2.500%
	0.400	0.41	2.500%
average	0.400	0.41	** 2.500%
2	0.800	0.80	0.000%
	0.800	0.80	0.000%
	0.800	0.80	0.000%
average	0.800	0.80	** 0.000%
3	1.200	1.20	0.000%
	1.200	1.20	0.000%
	1.200	1.20	0.000%
average	1.200	1.20	** 0.000%
4	1.600	1.60	0.000%
	1.600	1.60	0.000%
	1.600	1.60	0.000%
average	1.600	1.60	** 0.000%
5	2.000	2.00	0.000%
	2.000	2.00	0.000%
	2.000	2.00	0.000%
average	2.000	2.00	** 0.000%

**STANDARD CORRECTION FACTOR**  
 AVERAGE DEVIATION  
 STANDARD DEVIATION  
 95% CONFIDENCE INTERVAL  
 PRECISION( within +/- 3%)

0.995
0.005
0.010
0.025
-0.99

† If pressure or vacuum decreases by more than 1 in. in 5 minutes then remove from service.  
 †† If pressure or vacuum decreases by more than 5% in 5 minutes then remove from service.  
 \*\* These values must be within +/- 5% before the magnehelic can be put into operation.

Calibration by: RTR

Reviewed by: CDD

### MAGNEHELIC CALIBRATION

DATE: 7/27/90  
 GAGE ID # M-11  
 RANGE 0-1.0 in. H2O

SCHEDULED CALIBRATION:  
 SEMI-ANNUAL   
 BI-MONTHLY   
 OTHER

REFERENCE ID # DWYER 0-10 MANO

**LEAK CHECK:**

System:	† Set @ 10 in. H2O	vacuum 10 in. P F	pressure 10 in. P F
Point:	†† Set @ 90 % FS in. H2O	vacuum in. P F	pressure in. P F

Point	Incline Delta P Pinc	Magnehelic Delta P Pmag	% Deviation (Pinc-Pmag)/Pinc x 100
1	0.200	0.20	0.000%
	0.200	0.19	5.000%
	0.200	0.20	0.000%
average	0.200	0.20	** 1.667%
2	0.400	0.40	0.000%
	0.400	0.40	0.000%
	0.400	0.40	0.000%
average	0.400	0.40	** 0.000%
3	0.600	0.60	0.000%
	0.600	0.60	0.000%
	0.600	0.60	0.000%
average	0.600	0.60	** 0.000%
4	0.800	0.80	0.000%
	0.800	0.80	0.000%
	0.800	0.80	0.000%
average	0.800	0.80	** 0.000%
5	1.000	1.00	0.000%
	1.000	1.00	0.000%
	1.000	1.00	0.000%
average	1.000	1.00	** 0.000%

**STANDARD CORRECTION FACTOR**

AVERAGE DEVIATION  
 STANDARD DEVIATION  
 95% CONFIDENCE INTERVAL  
 PRECISION( within +/- 3%)

1.003
0.003
0.012
0.031
-1.00

† If pressure or vacuum decreases by more than 1 in. in 5 minutes then remove from service.  
 †† If pressure or vacuum decreases by more than 5% in 5 minutes then remove from service.  
 \*\* These values must be within +/- 5% before the magnehelic can be put into operation.

Calibration by: RTR

Reviewed by: \_\_\_\_\_

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### MAGNEHELIC CALIBRATION

DATE: 7/27/90  
 GAGE ID # M-12  
 RANGE 0-2 in. H2O

SCHEDULED CALIBRATION:  
 SEMI ANNUAL   
 BI-MONTHLY   
 OTHER

REFERENCE ID # 0-10 DWYER MANO

**LEAK CHECK:**

System:	† Set @ 10 in. H2O	vacuum 10 in. P F	pressure 10 in. P F
Point:	†† Set @ 90 % FS in. H2O	vacuum in. P F	pressure in. P F

Point	Incline Delta P <i>Pinc</i>	Magnehelic Delta P <i>Pmag</i>	% Deviation $(Pinc - Pmag) / Pinc \times 100$
1	0.400	0.45	12.500%
	0.400	0.45	12.500%
	0.400	0.45	12.500%
average	0.40	0.45	** 12.500%
2	0.800	0.85	6.250%
	0.800	0.85	6.250%
	0.800	0.85	6.250%
average	0.80	0.85	** 6.250%
3	1.200	1.23	2.500%
	1.200	1.23	2.500%
	1.200	1.24	3.333%
average	1.20	1.23	** 2.778%
4	1.600	1.62	1.250%
	1.600	1.63	1.875%
	1.600	1.64	2.500%
average	1.60	1.63	** 1.875%
5	2.000	2.05	2.500%
	2.000	2.05	2.500%
	2.000	2.05	2.500%
average	2.00	2.05	** 2.500%

**STANDARD CORRECTION FACTOR**

AVERAGE DEVIATION  
 STANDARD DEVIATION  
 95% CONFIDENCE INTERVAL  
 PRECISION( within +/- 3%)

0.952
0.052
0.040
0.099
-0.90

† If pressure or vacuum decreases by more than 1 in. in 5 minutes then remove from service.  
 †† If pressure or vacuum decreases by more than 5% in 5 minutes then remove from service.  
 \*\* These values must be within +/- 5% before the magnehelic can be put into operation.

Calibration by: RTR

Reviewed by: \_\_\_\_\_

### MAGNEHELIC CALIBRATION

DATE: 7/27/90  
 GAGE ID # M-7  
 RANGE 0-5 in. H2O

SCHEDULED CALIBRATION:  
 SEMI ANNUAL   
 BI-MONTHLY   
 OTHER

REFERENCE ID # 0-10 DWYER MANO

**LEAK CHECK:**

System:	† Set @ 10 in. H2O	vacuum 10 in. P F	pressure 10 in. P F
Point:	†† Set @ 90 % FS in. H2O	vacuum in. P F	pressure in. P F

Point	Incline Delta P Pinc	Magnehelic Delta P Pmag	% Deviation (Pinc-Pmag)/Pinc x 100
1	1.000	0.95	5.000%
	1.000	0.95	5.000%
	1.000	0.95	5.000%
average	1.00	0.95	** 5.000%
2	2.000	2.05	2.500%
	2.000	2.00	0.000%
	2.000	2.00	0.000%
average	2.00	2.02	** 0.833%
3	3.000	3.05	1.667%
	3.000	3.05	1.667%
	3.000	3.05	1.667%
average	3.00	3.05	** 1.667%
4	4.000	4.00	0.000%
	4.000	4.00	0.000%
	4.000	4.00	0.000%
average	4.00	4.00	** 0.000%
5	5.000	4.95	1.000%
	5.000	4.95	1.000%
	5.000	4.95	1.000%
average	5.00	4.95	** 1.000%

**STANDARD CORRECTION FACTOR**  
 AVERAGE DEVIATION  
 STANDARD DEVIATION  
 95% CONFIDENCE INTERVAL  
 PRECISION( within +/- 3%)

1.008
0.017
0.018
0.045
-0.99

† If pressure or vacuum decreases by more than 1 in. in 5 minutes then remove from service.  
 †† If pressure or vacuum decreases by more than 5% in 5 minutes then remove from service.  
 \*\* These values must be within +/- 5% before the magnehelic can be put into operation.

Calibration by: RTR

Reviewed by: \_\_\_\_\_

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1536 Eastman Avenue  
Ventura, CA 93003  
(805) 644-1095

BILL TO Company:

Address:

CHAIN OF CUSTODY RECORD

Phone #: ( ) - ( ) Contact:

PROJ. NO.	PROJECT NAME	NO.	DATE	TIME	SAMPLE I.D.	NO. OF CONTAINERS	REMARKS	CHECK IF RUSH
99	12390	✓			Run 1 PM10 - 10 rinses "Suction"			
100					+ 10 rinses			
101					Filters - X-38, X-37, J			
102					Run 1 Part Imps Suction"			
103					Probe			
104					Filter D-20			
105					Run 2 Suction PM10 - 10 rinses			
106					+ 10 rinses			
107					Filters F-1, X-35, X-36.			
108					Run 2 Suction Part Imps.			
109					Probe			
110					Filter D-21			
111					Run 1 Dryer PM10 - 10 rinses			
112					+ 10 rinses			
113					Filters F-2, X-32, X-38			

*Analysis*  
*Mass Spectrometry*

The undersigned hereby acknowledges having received a copy of the Fee Schedule/General Information and Conditions, the provisions of which are a part of this agreement.

Relinquished by: (Signature)	Date/Time	Received by: (Signature)	Date/Time
Relinquished by: (Signature)	Date/Time	Received for Laboratory by: (Signature)	Date/Time
NAME		ADDRESS	
PHONE NO.		PHONE NO.	

WHITE COPY \_\_\_\_\_ CANARY COPY \_\_\_\_\_ PINK COPY \_\_\_\_\_



1536 Eastman Avenue  
Ventura, CA 93003  
(805) 644-1095

BILL TO Company:  
Address:

CHAIN OF CUSTODY RECORD

Phone #: ( ) Contact:

PROJ. NO.	PROJECT NAME	NO.	DATE	TIME	COMP	GRAB	SAMPLE ID.	NO. OF CONTAINERS	REMARKS	CHECK IF RUSH
40188	Eckley-Hanford									
SAMPLERS: (Signature) <i>[Signature]</i>										
114	12-3-80						Run Dryer Part Imps.			
115							Probs			
116							Filter D-22			
117							Run 2 Dryer PM10 -10 rins			
118							+10 rins			
119							Filters F-3, X-9, X-40			
120							Run 2 Dryer Part Imps			
121							Probs			
122							Filter D-23			
123	12-4-90						Run 1 Mate PM10 -10 rins			
124							+10 rins			
125							Filters F-4, X-4, X-2			
126							Run 1 Mate Part Imps			
127							Probs			
128							Filter D-24			

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Relinquished by: (Signature)	Date/Time	Received by: (Signature)	Date/Time	Relinquished by: (Signature)	Date/Time	Received by: (Signature)	Date/Time
Relinquished by: (Signature)	Date/Time	Received for Laboratory by: (Signature)	Date/Time	NAME ADDRESS	PHONE NO.		



1536 Eastman Avenue  
Ventura, CA 93003  
(805) 644-1095

BILL TO Company:

Address:

CHAIN OF CUSTODY RECORD

Phone #: ( ) Contact:

PROJ. NO.	PROJECT NAME	NO.	DATE	TIME	COMP	GRB	SAMPLE I.D.	NO. OF CONTAINERS	REMARKS	CHECK IF RUSH
40-188	Eckley - Hanford	129	12-4-90		✓		Run 2 Motc PM10 - 10 rings			
		130					+ 10 rinse			
		131					Filters FS-X-43, X-44			
		132					Run 2 Motc Part Imps			
		133					Probe			
		134					Filter D-25			
		135					Run 1 Hint Trap PM10-10			
		136					+ 10 rinse			
		137					Filters F-6, X-45, X-46			
		138					Run 1 Hint Trap Part Imps			
		139					Probe			
		140					Filter D-26			
		141					Run 1 Hint Trap PM10-10			
		142					+ 10 rinse			
		143					Filters F-7, X-47, X-48			

The undersigned hereby acknowledges having received a copy of the Fee Schedule/General Information and Conditions, the provisions of which are a part of this agreement.

Relinquished by: (Signature)	Date/Time	Received by: (Signature)	Date/Time	Relinquished by: (Signature)	Date/Time	Received by: (Signature)	Date/Time
Relinquished by: (Signature)	Date/Time	Received for Laboratory by: (Signature)	Date/Time	NAME	ADDRESS	PHONE NO.	

WHITE COPY \_\_\_\_\_ CANARY COPY \_\_\_\_\_ PINK COPY \_\_\_\_\_

