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AP-42 Section Number: 9.9.1

Reference Number: 30

**Title: Report of Particulate Emission
Tests For Wayne Farms Laurel
Feed Mill**

Environmental Monitoring Lab.

August 29 and September 20, 1994

REPORT OF
PARTICULATE EMISSIONS TESTS
FOR
WAYNE FARMS
LAUREL FEED MILL

Laurel, Mississippi
August 29 and September 20, 1994

Wayne Farms
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September 27, 1994

Subject: Wayne Farms -- Laurel Feed Mill
Laurel, Mississippi

On August 29 and September 20, 1994, Environmental Monitoring Laboratories performed air emissions testing for Wayne Farm's feed mill in Laurel, Mississippi. Testing was performed to measure particulate (PM) emissions from the pouring aspiration - *(HAMMILL) GRINDER* cyclone stack and the cooler cyclone stack in accordance with requirements of the Mississippi Department of Environmental Quality.

Test results:

	PARTICULATE EMISSIONS	
	pounds/hr	grains/dscf
POURING ASPIRATION STACK <i>(HAMMILL GRINDER)</i>	0.04	0.002
COOLER STACK	5.00	0.021

The testing project was coordinated by Mr. Greg Bull of Wayne Farms. Rodney Moore of Environmental Monitoring Laboratories was responsible for sample collection and delivery. Danny Russell of EML was responsible for sample analysis and for report preparation. Sample custody was limited to Mr. Russell.

Following is a report of the test.

REPORT OF PARTICULATE EMISSIONS TEST FOR
WAYNE FARMS
LAUREL FEED MILL
LAUREL, MISSISSIPPI
AUGUST 29 AND SEPTEMBER 20, 1994

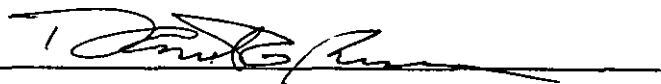
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REPORT CERTIFICATION

I certify that I have examined the information submitted herein,
and based upon my inquiries of those responsible for obtaining the
data or upon my direct acquisition of data, I believe the submitted
information is true, accurate and complete.

Signed



Daniel G. Russell

1.0 Test Results:

The following tables present the measured flow parameters and test results for particulate emissions testing done on August 29 and September 20, 1994. for Wayne Farms' feed mill in Laurel, Mississippi.

1.1 Pouring Aspiration Cyclone Stack

Run No.		1	2	3	AVG.
Date		8/29/94	8/29/94	8/29/94	—
Time Start		1315	1421	1529	—
Time End		1416	1522	1630	—
Particulate Emissions	#/hr	0.04	0.02	0.05	0.04
Particulate Emissions	gr/dscf	0.002	0.001	0.003	0.002
Volumetric Flowrate	acfm	2377	2411	2494	2428
Volumetric Flowrate	dscfm	2099	2143	2203	2148
Velocity	ft./sec.	31.5	31.9	33.0	32.1
Stack Temperature	°F	112	113	113	113
Moisture	%	4.3	3.4	4.1	3.9
Sample Rate	% isokinetic	104	103	100	102

1.2 Cooler Stack

Run No.		1	2	3	AVG.
Date		9/20/94	9/20/94	9/20/94	—
Time Start		1011	1236	1424	—
Time End		1112	1337	1525	—
Particulate Emissions	#/hr	4.10	7.27	3.62	5.00
Particulate Emissions	gr/dscf	0.018	0.028	0.018	0.021
Volumetric Flowrate	acfm	32115	34523	28712	31783
Volumetric Flowrate	dscfm	26953	30255	23348	26852
Velocity	ft./sec.	49.6	53.3	44.3	49.0
Stack Temperature	°F	112	98	118	109
Moisture	%	6.7	4.9	8.6	6.7
Sample Rate	% isokinetic	104	100	105	103

2.0 SOURCE DESCRIPTION: Source description here is limited to a description of the sampling locations. Process descriptions and records of operating conditions during the test may be requested of Wayne Farms.

The pouring aspiration cyclone exhausts to the atmosphere by way of a rectangular stack measuring 14.5 inches by 12.5 inches. A slot for sampling was installed at a location that is 21 inches below a vertical to horizontal elbow, and 48 inches above a horizontal to vertical elbow.

The cooler stack exhausts to the atmosphere by way of a 44.5 inch diameter stack. Sampling was performed in a vertical section of the stack at a location that is 258 inches (5.7 diameters) below an elbow, and 288 inches (6.4 diameters) above a horizontal to vertical elbow.

3.0 TEST PROCEDURES: Test procedures used are those described in the Code of Federal Regulations, Title 40, Part 60, Appendix A. Specifically, Method 1 was used to determine the number of sample points, and Method 5 to determine flow rates, moisture content, and particulate emissions. The sampling train used is identical to that described in Method 5 except that the cyclone was omitted. Sample duration was 60 minutes for each of three runs.

Filters were recovered by rinsing the front half of the filter holder into the probe wash and securing the filters in glass petri dishes. Part of the sample filter normally adheres to the filter gasket, and some of the adhering material is recovered into the probe wash. Therefore some of the filter weight is attributed to the probe wash weight. Filters were heated in an oven for 2 hours at 105° C, desiccated at least 24 hours and weighed to constant weight. Probe wash samples in acetone were evaporated to dryness over low heat in tarred beakers, desiccated for at least 24 hours and weighed to constant weight. Weighings are made at 6 hour or greater intervals (samples stored in desiccator). Final weights are considered valid and are recorded if there is no more than 0.5 milligrams difference from the previous weighing

4.0 DATA REDUCTION

Wayne Feeds - Laurel Feedmill
 Pouring Aspiration Cyclone Stack
 Particulate Emissions Test - August 29, 1994

Collected Test
 Data:

RUN 1 RUN 2 RUN 3

Date :	8/29/94	8/29/94	8/29/94
Time start :	1315	1421	1529
Time end :	1416	1522	1630
1. As : sq ft	1.2587	1.2587	1.2587
2. Dn : in.	0.275	0.275	0.275
3. Cp : dimensionless	0.84	0.84	0.84
4. Theta : minutes	60.00	60.00	60.00
5. Y : dimensionless	1.00	1.00	1.00
6. Pbar : in. Hg	29.90	29.90	29.90
7. Pg : in. H2O	-0.05	-0.05	-0.05
8. Vm : cf (dry gas)	45.543	46.234	45.934
9. $\text{sqr}(\text{DP})_{\text{avg}}$: in.H2O ^{.5}	0.5338	0.5417	0.5598
10. DH : in. H2O	1.7875	1.8396	1.8042
11. ts : degrees F	112.04	113.21	113.04
12. tm : degrees F	104.06	105.67	104.81
13. Vlc : ml	40.5	32.5	39
14. CO2 : percent	0.00	0.00	0.00
15. O2 : percent	20.90	20.90	20.90
16. CO : percent	0.00	0.00	0.00
17. M,PM : milligrams	6.5	3.5	7.4

112.76

Wayne Feeds - Laurel Feedmill
 Pouring Aspiration Cyclone Stack
 Particulate Emissions Test - August 29, 1994

Calculations:

		RUN 1	RUN 2	RUN 3	AVG.
1. Pm	: in.Hg (DH/13.6)+Pbar	30.0314	30.0353	30.0327	
2. Ps	: in. Hg (Pg/13.6)+Pbar	29.8963	29.8963	29.8963	
3. An	: sq ft ((Dn/24)^2)(3.1416)	4.12E-04	4.12E-04	4.12E-04	
4. Vmstd	: dscf Vm Y(Pm/Pstd)(Tstd/Tm)	42.790	43.321	43.102	43.071
5. Vwstd	: scf (.04707cf/ml)(Vlc)	1.906	1.530	1.836	
6. Bws	: dimensionless Vwstd/(Vwstd+Vmstd)	0.0427	0.0341	0.0409	0.0392
7. Md	: mol.wt. dry basis .44 CO2+.32 O2+.28(CO+N2)	28.84	28.84	28.84	
8. Ms	: mol.wt. wet basis Md(1-Bws)+18 Bws	28.37	28.47	28.39	
9. Vs	: ft/sec Kp Cp (sqrDP)sqr(Ts/(Ps Ms))	31.48	31.93	33.03	32.14
10. Q	: cfm Vs As(60 sec/min)	2377	2411	2494	2428
11. Qstw	: scfm Q(Ps/Pstd)(Tstd/Ts)	2193	2219	2297	2236
12. Qstd	: dscfm Qstw(1-Bws)	2099	2143	2203	2148
13. I	: percent [(100 Ts)(.002669 Vlc+(Vm Pm/Tm))/(60 theta Vs Ps An)	103.68	102.80	99.52	102.00

Particulate Emissions

14. E,PM	: pounds/hr (M,PM/Vmstd)(Qstd)(60)/(453590)	0.04	0.02	0.05	0.04
15. C,PM	: grains/dscf (M,PM/Vmstd)(.0154 grains/mg)	0.002	0.001	0.003	0.002

Wayne Feeds - Laurel Feedmill
Cooler Stack
Particulate Emissions Test - September 20, 1994

Collected Test
Data:

RUN 1

RUN 2

RUN 3

Date :	9/20/94	9/20/94	9/20/94
Time start :	1011	1236	1424
Time end :	1112	1337	1525
¹ As : sq ft	10.8006	10.8006	10.8006
² Dn : in.	0.250	0.250	0.250
³ Cp : dimensionless	0.84	0.84	0.84
⁴ Theta : minutes	60.00	60.00	60.00
⁵ Y : dimensionless	1.01	1.01	1.01
⁶ Pbar : in. Hg	29.78	29.78	29.78
⁷ Pg : in. H2O	-8.5	-8.5	-8.5
⁸ Vm : cf (dry gas)	55.418	60.430	49.546
⁹ sqrt(DP),avg : in.H2O ^{.5}	0.8261	0.9020	0.7318
¹⁰ DH : in. H2O	2.5275	3.1275	2.0050
¹¹ ts : degrees F	111.90	98.15	118.30
¹² tm : degrees F	98.25	104.80	107.95
¹³ Vlc : ml	81	63	93
¹⁴ CO2 : percent	0.00	0.00	0.00
¹⁵ O2 : percent	20.90	20.90	20.90
¹⁶ CO : percent	0.00	0.00	0.00
¹⁷ M,PM : milligrams	61	103.9	54.5

109.45

Wayne Feeds - Laurel Feedmill
Cooler Stack
Particulate Emissions Test - September 20, 1994

Calculations:		RUN 1	RUN 2	RUN 3	AVG.
1.	Pm : in.Hg (DH/13.6)+Pbar	29.9658	30.0100	29.9274	
2.	Ps : in. Hg (Pg/13.6)+Pbar	29.1550	29.1550	29.1550	
3.	An : sq ft ((Dn/24)^2)(3.1416)	3.41E-04	3.41E-04	3.41E-04	
4.	Vmstd : dscf Vm Y(Pm/Pstd)(Tstd/Tm)	53.020	57.229	46.533	52.261
5.	Vwstd : scf (.04707cf/ml)(Vlc)	3.813	2.965	4.378	
6.	Bws : dimensionless Vwstd/(Vwstd+Vmstd)	0.0671	0.0493	0.0860	0.0674
7.	Md : mol.wt. dry basis .44 CO2+.32 O2+.28(CO+N2)	28.84	28.84	28.84	
8.	Ms : mol.wt. wet basis Md(1-Bws)+18 Bws	28.11	28.30	27.90	
9.	Vs : ft/sec Kp Cp (sqrDP)sqr(Ts/(Ps Ms))	49.56	53.27	44.31	49.05
10.	Q : cfm Vs As(60 sec/min)	32115	34523	28712	31783
11.	Qstw : scfm Q(Ps/Pstd)(Tstd/Ts)	28892	31823	25545	28753
12.	Qstd : dscfm Qstw(1-Bws)	26953	30255	23348	26852
13.	I : percent [(100 Ts)(.002669 Vlc+(Vm Pm/Tm))/(60 theta Vs Ps An)	103.88	99.89	105.25	103.01

Particulate Emissions

14.	E,PM : pounds/hr (M,PM/Vmstd)(Qstd)(60)/(453590)	4.10	7.27	3.62	5.00
15.	C,PM : grains/dscf (M,PM/Vmstd)(.0154 grains/mg)	0.018	0.028	0.018	0.021

5.0 NOMENCLATURE

SYMBOL	UNITS	DESCRIPTION
A_n	ft^2	Nozzle cross sectional area
A_s	ft^2	Stack cross sectional area
B_{ws}	dimensionless	Wet gas fraction
CO_2	percent	Carbon dioxide content by volume
CO	percent	Carbon monoxide content by volume
C_p	dimensionless	Pitot correction factor
C_X	as labeled	Concentration of pollutant X
DGF	dimensionless	Dry gas fraction
D_n	inches	Nozzle diameter
ΔH	in. H_2O	Pressure drop across meter orifice
ΔP	in. H_2O	Stack gas velocity pressure
E_X	$\#/\text{hr}$	Emission rate of pollutant X
EX	$\#/\text{MM Btu}$	Emission rate of pollutant X
F	dscf	Volume of flue gas per MM Btu
I	percent	Nozzle velocity/stack gas velocity
K_p	consistent	Pitot tube constant
M_X	milligrams	Sample weight of pollutant X
M_d	$\#/\# \text{ mole}$	Dry molecular weight of stack gas
M_s	$\#/\# \text{ mole}$	Wet molecular weight of stack gas
N_2	percent	Nitrogen content by volume, dry basis
O_2	percent	Oxygen content by volume, dry basis
P_{bar}	in. Hg	Barometric pressure
P_g	in. Hg	Stack static pressure
P_m	in. Hg	Total pressure at meter ($P_{bar} + (\Delta H/13.6)$)
P_s	in. Hg	Total stack pressure ($P_{bar} + (P_g/13.6)$)
P_{std}	in. Hg	Standard barometric pressure = 29.92
Q	acfm	Volumetric flow rate at stack conditions
Q_{std}	dscfm	Volumetric flow rate at standard conditions, dry basis
Q_{stdw}	scfm	Volumetric flow rate at standard conditions, wet basis
θ	minutes	Sample duration
t_m	$^{\circ}\text{F}$	Meter temperature (T_m denotes $^{\circ}\text{R}$)
t_s	$^{\circ}\text{F}$	Stack temperature (T_s denotes $^{\circ}\text{R}$)
T_{std}	$^{\circ}\text{R}$	Standard temperature = 528 $^{\circ}\text{R}$
V_{lc}	ml	volume of water collected
V_m	ft^3	Volume of dry gas sampled through meter
V_{mstd}	dscf	Sample volume at standard conditions
V_{wstd}	scf	Sample volume of water vapor
Y	dimensionless	Meter coefficient
X_{sair}	percent	Excess air

7.0 APPENDICES

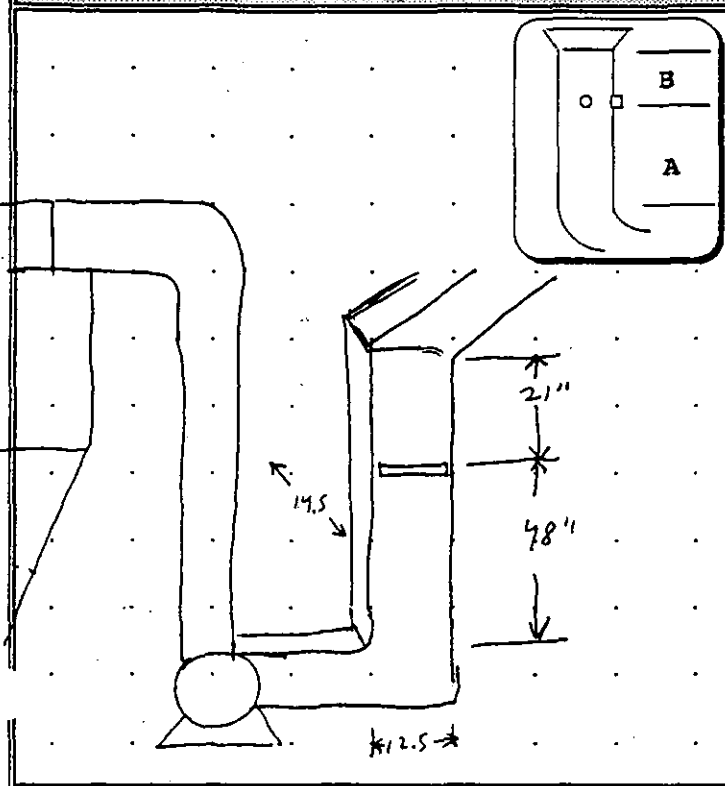
A. Field and Analytical Data

B. Calibrations

STACK CONFIGURATION AND SAMPLE POINT LAYOUT FOR CIRCULAR STACKS

PLANT: Wayne Farms - Laurel Feedmill Date: 8-29-94
SOURCE: Pauling Aspiration Stock
TEST FOR: PM
TEST OPERATORS: Mason / G. McKnight

SKETCH OF SUBJECT



PERCENT OF DIAMETER

[illegible]

STACK DIAMETER: 14.5×12.5 $D_e = 13.43$

Distance from ports to disturbance:

A. to upstream disturbance

B. to downstream disturbance

Upstream diameters:

Downstream diameters:

Minimum No. sample points required:

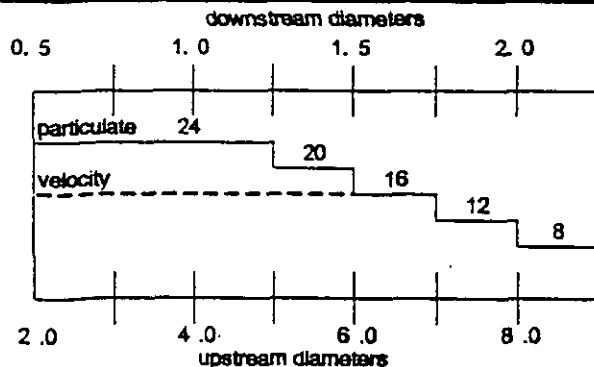
No. sample points selected:

Port Length:

Port Type:

Port Access:

MINIMUM NO. OF POINTS ON A DIAMETER

[illegible]

Pitot ID : _____ Pitot Cp: _____ Stack Temp: _____

Remarks: _____

Plant Wayne Farms Feedmill
 Sampling Location Pouring Operation Stack
 Test For PM
 Test Operators Mon/6. McEwen
 RUN No. 1
 Date 8-29-94
 Time start 1315 end 1416

Meter Box ALC
 Sample Box 40.4
 Probe/Pitot 4' in
 Pitot Cp .84
 Nozzle Dia. 275
 Filter No.

No. Sample Pts. 6x4
 Minutes/Pt. 2.5

NOMOGRAPH

$\Delta H @$ 1.90
 Meter Temp. 110
 % H₂O 510
 C-Factor 105
 Stack Temp. 110
 Ref. ΔP 30

Gas Analysis

CO₂ 412
 O₂
 CO
 Time

Condensate:

tare 200 fin 231
 Silica gel:
 tare 713 fin 722.5

Remarks:

Port Point	El. Time, Min.	DGM Reading, Ft.	Velocity Head ΔP , in. H ₂ O	Orifice ΔH , in. H ₂ O	Stack Temp. °F	Meter Temp., °F In Out	Oven Temp. °F	Imp. Temp. °F	Vac in. Hg
1	000	362 4 81	0 20	1 25	1019	96 96	44	55	2
2	230	364 2	0 25	1 55	1018	97 96		56	2
3	500	365 9	0 24	1 50	110	101 97		57	2
4	730	367 2	0 29	1 80	110	105 100		58	2
5	1000	369 5	0 34	2 10	109	103 97		58	2
6	1200	371 6	0 34	2 10	100	106 96		59	2
1	1500	373 6 51	0 23	1 45	111	107 103		56	2
2	230	375 4	0 26	1 60	115	109 100		58	2
3	500	377 2	0 27	1 65	117	109 102		57	2
4	730	379 0	0 30	1 85	115	109 102		60	2
5	1000	381 0	0 31	1 95	115	110 100		62	2
6	1200	383 0	0 35	2 20	114	111 101		64	2
1	3000	385 9 98	0 27	1 70	113	111 101		68	2
2	230	386 9	0 28	1 75	114	113 103		65	2
3	500	388 8	0 28	1 75	114	111 102		69	2
4	730	390 6	0 32	2 00	110	109 102		70	2
5	1100	392 6	0 32	2 00	110	109 101		68	2
6	1230	394 5	0 35	2 20	109	107 101		69	2
1	1500	396 7 29	0 23	1 45	108	114 104		69	2
2	230	398 4	0 18	1 10	112	111 103		65	2
3	500	400 0	0 28	1 75	114	110 103		62	2
4	730	401 9	0 29	1 80	113	108 101		66	2
5	1000	403 9	0 34	2 10	112	107 100		67	2
6	1230	405 9	0 37	2 30	112	108 103		69	2
28	out 60/12	408 0 24							

Leak: 0.4 — 0.071 — 0.007 at 8 11/16

455930 5338 1.7825 112.04 104.06

Plant Wayne Farms, Inc. Lancaster
 Sampling Location Aspiration Peering Aspiration Stack
 Test For PM
 Test Operators Wesley G. McKnight

RUN No. 2
 Date 8-29-90
 Time start 1421 end 1522

Meter Box AdC
 Sample Box No. 3
 Probe/Pitot 4' box
 Pitot Cp 275.84
 Nozzle Dia. 2.75
 Filter No. _____
 Amb. Temp. °F 93
 Bar. Press. "Hg _____
 Static Press. "H₂O -0.5

No. Sample Pts. 8x4
 Minutes/Pt. 2.5
 NOMOGRAPH
 ΔH@ 1.90
 Meter Temp. 110
 % H₂O 4.0
 C-Factor 1.05
 Stack Temp. 110
 Ref. ΔP 30

Gas Analysis
 CO₂ _____
 O₂ _____
 CO _____
 Time _____
 Condensate:
 tare 200 fin 225
 Silica gel:
 tare 703 fin 780.5

Remarks:

Port Point	El. Time. Min.	DGM Reading. Ft.	Velocity Head ΔP. in. H ₂ O	Orifice ΔH in. H ₂ O	Stack Temp. °F	Meter Temp. °F In	Meter Temp. °F Out	Oven Temp. °F	Imp. Temp. °F	Vac. in. Hg
1	210	408	414	0.16	1.00	113	104	100	69	2
2	230	409	9	0.24	1.50	111	106	104	65	2
3	500	411	7	0.30	1.85	111	106	101	64	2
4	770	413	6	0.34	2.10	113	109	101	62	2
5	1000	415	6	0.36	2.25	115	107	101	62	2
6	1230	417	8	0.36	2.25	117	111	97	64	2
1	1500	419	8.51	0.27	1.65	111	110	102	65	2
2	230	421	7	0.26	1.60	114	111	104	66	2
3	500	423	5	0.28	1.75	113	111	103	67	2
4	770	425	4	0.30	1.85	114	111	101	68	2
5	1000	427	3	0.33	2.05	112	111	103	65	2
6	1230	429	3	0.38	2.40	114	112	102	64	2
1	2000	431	5.57	0.26	1.60	113	107	101	62	2
2	230	433	4	0.26	1.60	114	111	102	61	2
3	500	435	2	0.28	1.75	113	109	102	60	2
4	770	437	1	0.31	1.95	115	110	104	61	2
5	1000	439	1	0.34	2.10	115	112	105	63	2
6	1230	441	2	0.36	2.25	114	111	104	64	2
1	1450	443	2.30	0.24	1.50	113	109	101	65	2
2	230	445	1	0.24	1.50	115	111	100	66	2
3	500	446	7	0.26	1.60	112	109	101	69	2
4	770	448	6	0.29	1.80	113	111	100	70	2
5	1000	450	5	0.32	2.00	114	111	102	70	2
6	1230	452	4	0.36	2.25	112	111	101	70	2
1	1400	454	6.48							
Sample: 929 — 0.076 — 0.07 (X) 8 (H) P ₁ + 4.0 9.5 P ₂ — 2 9.6 46.2340 5417 1.8396 113.21 10567										

Plant Wayne Farms admitt Liquor
 Sampling Location Bearing Aspiration Stack
 Test For PM
 Test Operators None / G. McKnight

RUN No. 3
 Date 8-29-94
 Time start 1529 end 1630

Meter Box ASC
 Sample Box No. 4
 Probe/Pitot 4' an
 Pitot Cp .94
 Nozzle Dia. .275
 Filter No.

No. Sample Pts. 6x4
 Minutes/Pt. 2.5

Gas Analysis
 CO₂
 O₂
 CO
 Time

Remarks:

Amb. Temp. °F 94
 Bar. Press. "Hg
 Static Press. "H₂O -.05

NOMOGRAPH
 ΔH@ 1.90
 Meter Temp. 110
 % H₂O <10
 C-Factor 1.05
 Stack Temp. 110
 Ref. ΔP .30

Condensate:
 tare 200 fin 232
 Silica gel:
 tare 722.5 fin 729.5

Port Point	El. Time, Min.	DGM Reading, Ft.	Velocity Head Δ P, in. H ₂ O	Orifice Δ H in. H ₂ O	Stack Temp. °F	Meter Temp., °F In Out	Oven Temp. °F	Imp. Temp. °F	Vac in. Hg	
1	000	45.5	1.09	0.24	115.0	112	104	100	60	3
2	230	45.6	.9	0.26	116.0	114	107	100	62	3
3	500	45.8	.7	0.28	117.5	116	104	100	63	3
4	730	46.0	.6	0.30	118.5	114	109	103	62	3
5	1000	46.2	.5	0.34	2.10	113	105	100	64	3
6	1230	46.4	.5	0.37	2.50	115	110	101	62	3
1	5100	46.6	.768	0.36	1.60	114	107	100	63	3
2	230	46.7	.6	0.26	1.60	114	108	100	63	3
3	500	47.0	.3	0.20	1.60	111	105	99	63	3
4	730	47.2	.0	0.30	1.85	114	108	101	63	3
5	6000	47.4	.1	0.31	1.95	115	110	106	63	3
6	1230	47.6	.5	0.25	1.55	114	111	101	64	3
1	30000	47.8	.124	0.26	1.60	114	113	100	65	3
2	230	48.0	.3	0.26	1.60	113	111	100	68	3
3	500	48.2	.5	0.28	1.75	113	108	102	62	3
4	730	48.3	.6	0.28	1.75	113	112	103	68	3
5	1000	48.5	.5	0.32	2.00	114	113	104	66	3
6	1230	48.7	.4	0.34	2.10	114	111	102	68	3
1	45100	48.9	.530	0.24	1.50	114	111	100	65	3
2	230	49.1	.2	0.26	1.60	113	108	102	66	3
3	500	49.3	.1	0.27	1.70	113	110	103	68	3
4	730	49.5	.0	0.30	1.85	111	108	100	61	3
5	1000	49.6	.8	0.34	2.10	110	108	101	70	3
6	1230	49.8	.9	0.37	2.30	105	109	103	65	3
avg 60/100		50.1	.043							

2nd ch. 86.9 — 0.072 = .0030 Avg 9 1/2

45.9340 1.5598 1.8042 113.04 104.81

PAP PARTICULATE CATCH ANALYSIS

SAMPLES:

DATE TAKEN:

DELIVERED BY:

ANALYZED BY:

Wagner Foods - Laurel Feedmill

8-29-94 DATE ANALYZED: 9-7-94

RSM

RECEIVED BY: [Signature]

[Signature]

-Pomery
Aspartin
Stech

(Attach chain of custody if additional exchanges occur)

FILTERS:

RUN NO.	1	2	3		
FILTER NO.	2331	2329	2332		
FILTER TARE, gms.	5607	5610	5619		
	5630	5622	5650		
	5630	5621	5651		
FINAL WEIGHT, gms.	5630	5621	5651		
NET GAIN, gms.	.0023	.0011	.0032		

PROBE WASH:

RUN NO.	1	2	3		
CONTAINER ID.	Pom R1	Pom R2	Pom R3		
VOLUME INTACT?	✓	✓	✓		
VOLUME, ml	150	120	100		
TARE WEIGHT, gms.	(3) 104.6250	(67) 111.4662	(69) 112.5828		
	104.6294	111.4686	112.5874		
	104.6292	111.4686	112.5870		
FINAL WEIGHT, gms.	104.6292	111.4686	112.5870		
NET GAIN, gms.	.0042	.0024	.0042		
LESS BLANK, gms.					

PARTICULATE SAMPLE WEIGHT:

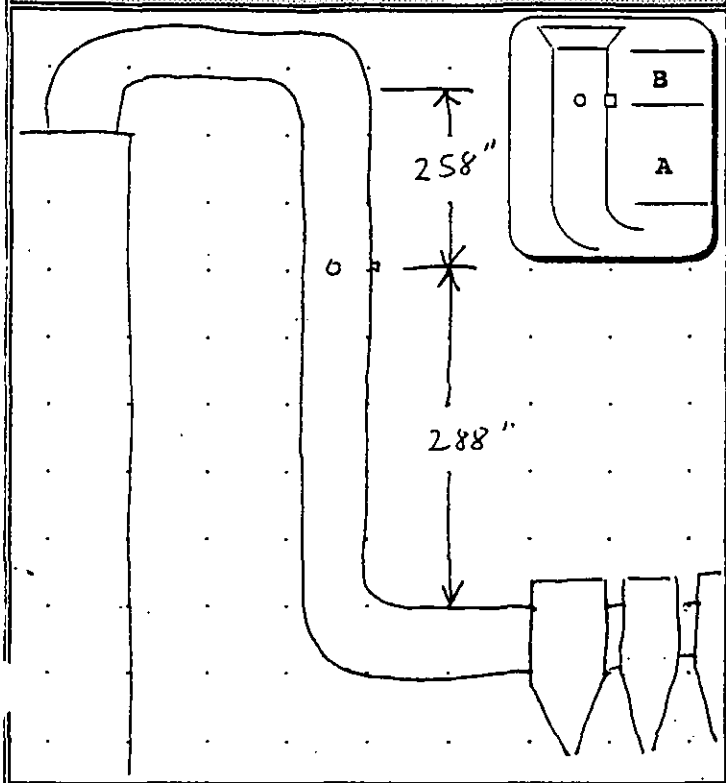
RUN NO.	1	2	3		
filter + probe, mg.	6.5	3.5	7.4		

STACK CONFIGURATION AND SAMPLE POINT LAYOUT FOR CIRCULAR STACKS

PLANT: Wayne Farms - Laurel Feedmill
SOURCE: Cooler Stack
TEST FOR: PM
TEST OPERATORS: Moore / G. McKnight

Date: 7-20-94

SKETCH OF STACK



PERCENT OF DIAMETER

	points on a diameter							
	2	4	6	8	10	12	14	16
point no.								
1	_____	14.6	6.7	4.4	3.2	2.6	2.1	1.6
2	_____	85.4	25.0	14.6	10.5	8.2	6.7	4.9
3	_____		75.0	29.6	19.4	14.6	11.8	9.9
4	_____		93.3	70.4	32.3	22.6	17.7	14.6
5	_____			85.4	67.7	34.2	25.0	20.1
6	_____			95.6	80.6	65.8	35.6	26.9
7	_____				89.5	77.4	64.4	38.6
8	_____				96.8	85.4	75.0	63.4
9	_____					91.8	82.3	73.1
10	_____					97.4	88.2	79.9
11	_____						93.3	85.4
12	_____						97.9	90.1
13	_____							94.3
14	_____							98.2
15	_____							95.1
16	_____							98.4

STACK DIAMETER:

Distance from ports to disturbance:

A. to upstream disturbance

B. to downstream disturbance

Upstream diameters:

Downstream diameters:

Minimum No. sample points required:

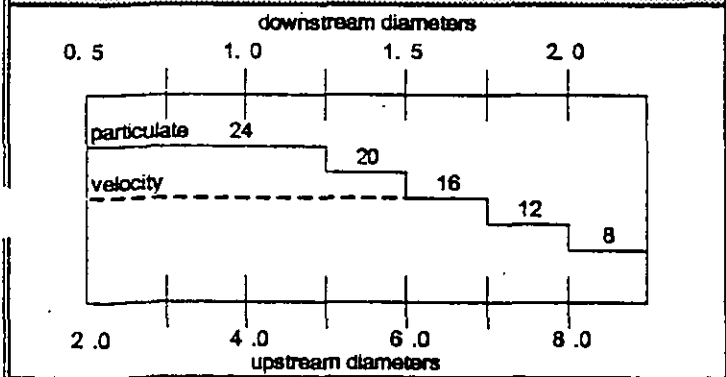
No. sample points selected:

Port Length:

Port Type:

Port Access:

MINIMUM NO. OF POINTS ON A DIAMETER



velocity head

[illegible]

Pitot ID : _____ Pitot Cp: _____ Stack Temp: _____

Remarks:

Plant Wayne Farms Laurel, N.C.
 Sampling Location Coaler Stack
 Test For PM
 Test Operators James L. McKnight
 RUN No. 1
 Date 9-20-94
 Time start 1011 end 1112

Meter Box <u>Anderson</u>	No. Sample Pts. <u>10x2</u>	Gas Analysis	Remarks:
Sample Box <u>No. 2</u>	Minutes/Pt. <u>30</u>	CO, _____	
Probe/Pitot <u>5 in</u>	NOMOGRAPH	O ₂ _____	
Pitot Cp <u>.84</u>	$\Delta H @$ <u>1.75</u>	CO _____	
Nozzle Dia. <u>.250</u>	Meter Temp. <u>100</u>	Time _____	
Filter No. _____	% H ₂ O <u>10</u>	Condensate:	
Amb. Temp. °F <u>70</u>	C-Factor <u>.93</u>	tare <u>200</u> fin <u>275</u>	
Bar. Press. "Hg <u>29.78</u>	Stack Temp. <u>120</u>	Silica gel:	
Static Press. "H ₂ O <u>-8.5</u>	Ref. ΔP <u>.50</u>	tare <u>729</u> fin <u>735</u>	

Port Point	El. Time, Min.	DGM Reading, Ft. ²	Velocity Head ΔP , in. H ₂ O	Orifice ΔH in. H ₂ O	Stack Temp. °F	Meter Temp., °F In Out	Oven Temp. °F	Imp. Temp. °F	Vac in. Hg
1	2:00	884.068	0.78	2.90	113	75 74	242	65	3
2	3	786.8	0.81	3.00	111	81 74	257	60	3
3	6	789.8	0.81	3.00	110	88 74	250	62	3
4	9	792.7	0.76	2.80	110	95 76	248	60	3
5	12	795.6	0.70	2.60	110	100 77	252	61	3
6	15	798.4	0.55	2.05	110	103 79	241	61	3
7	18	800.8	0.54	2.00	111	104 80	257	58	3
8	21	803.12	0.54	2.00	111	106 82	256	58	3
9	24	805.7	0.56	2.05	110	108 84	257	58	3
10	27	808.2	0.66	2.45	110	111 86	251	60	7
11									
12	30	810.989	0.67	2.45	109	108 88	250	60	2
13	3	813.8	0.77	2.85	112	116 90	251	62	3
14	6	816.8	0.68	2.55	113	119 92	228	60	3
15	9	819.6	0.63	2.25	114	121 94	230	60	3
16	12	822.3	0.57	2.10	115	121 86	258	62	3
17	15	824.8	0.67	2.45	115	122 97	242	65	3
18	18	827.6	0.76	2.80	115	125 98	248	64	7
19	21	830.5	0.73	2.65	115	127 99	251	65	3
20	24	833.4	0.76	2.80	112	128 101	256	66	7
21	27	836.3	0.76	2.80	112	129 102	260	67	7
22		839.486							
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Plant Wayne Farms Laurel, MS
 Sampling Location Cooler Stack
 Test For PM
 Test Operators Mon / L. McKnight
 RUN No. 2
 Date 9-20-94
 Time start 1226 end 1337

Meter Box <u>Amber</u>	No. Sample Pts. <u>10 x 2</u>	Gas Analysis	Remarks: <u>Duration: 11:25</u> <u>12:35</u> <u>1hr 10min</u>
Sample Box <u>10-4</u>	Minutes/Pt. <u>7.5</u>	CO ₂ _____	
Probe/Pitot <u>5' in</u>	NOMOGRAPH	O ₂ _____	
Pitot Cp <u>.87</u>	Δ H @ _____	CO _____	
Nozzle Dia. <u>.250</u>	Meter Temp. <u>100</u>	Time _____	
Filter No. _____	% H ₂ O <u>10</u>	Condensate:	
Amb. Temp. °F <u>74</u>	C-Factor <u>.97</u>	tare <u>200</u> fin <u>257</u>	
Bar. Press. "Hg <u>29.78</u>	Stack Temp. <u>120 / 100</u>	Silica gel:	
Static Press. "H ₂ O <u>-6.5</u>	Ref. Δ P <u>50 / .49</u>	tare <u>739</u> fin <u>745</u>	

Port Point	El. Time, Min.	DGM Reading, Ft.	Velocity Head Δ P, in. H ₂ O	Orifice Δ H, in. H ₂ O	Stack Temp. °F	Meter Temp., °F In	Meter Temp., °F Out	Oven Temp. °F	Imp. Temp. °F	Vac in. Hg
1	0.20	83.9	8.20	1.10	4.10	107	79	79	271	68
2	3	84.3	1	1.10	4.10	105	87	80	261	61
3	6	84.6	4	1.10	4.10	106	96	80	269	62
4	9	84.9	7	1.00	3.70	93	102	81	267	62
5	12	85.2	8	0.90	3.40	95	107	83	273	60
6	15	85.6	0	0.67	2.50	96	110	84	274	62
7	18	85.8	8	0.61	2.30	97	114	86	271	62
8	21	86.1	5	0.52	2.00	98	116	88	275	64
9	24	86.4	0	0.55	2.10	97	119	90	274	65
10	27	86.6	6	0.35	1.35	96	121	92	268	66
11	30/00	86.8	73.5	0.82	2.10	98	119	94	274	64
12	3	87.1	7	0.85	2.20	98	125	95	266	62
13	6	87.4	9	0.77	2.90	98	127	96	270	60
14	9	87.7	9	0.70	2.65	99	128	99	270	62
15	12	88.0	8	0.70	2.65	100	129	100	270	63
16	15	88.3	7	0.82	3.10	98	130	101	268	60
17	18	88.6	7	0.92	3.50	98	131	103	274	61
18	21	89.0	0	0.92	3.50	92	134	107	272	62
19	24	89.3	2	1.30	4.90	96	136	104	260	64
20	27	89.6	8	0.90	3.40	96	136	106	271	64
21		90.0	250							
22										
23										
24										
25										
26										
27										
28										
29										
30										
31										
32										
33										
34										
35										

Total ch. 027 → 0.33 = 0.06 CA-8 14.5
 4.9
 4.8
 60.430, 90.20, 3.1275, 98.15, 104.80

Plant Wayne Ferry Lake, MS
 Sampling Location Cooler Stack
 Test For PM
 Test Operators Moore, McKenney

RUN No. 3
 Date 9-20-84
 Time start 1407 and 1525
1424

Meter Box <u>ambuser</u>	No. Sample Pts. <u>10/2</u>	Gas Analysis	Remarks: <u>For downtime</u> <u>13:49</u> <u>14:05</u> <u>± 15 min</u>
Sample Box <u>10-2</u>	Minutes/Pt. <u>3.0</u>	CO ₂ _____	
Probe/Pitot <u>9' dia</u>	NOMOGRAPH	O ₂ _____	
Pitot Cp <u>.84</u>	ΔH@ <u>1.75</u>	CO _____	
Nozzle Dia. <u>.250</u>	Meter Temp. <u>100</u>	Time _____	
Filter No. _____	% H ₂ O <u>10</u>	Condensate:	
Amb. Temp. °F <u>78</u>	C-Factor <u>.93</u>	tare <u>200</u> fin <u>289</u>	
Bar. Press. "Hg <u>29.78</u>	Stack Temp. <u>100/120</u>	Silica gel:	
Static Press. "H ₂ O <u>-.05</u>	Ref. ΔP <u>.41 .50</u>	tare <u>732</u> fin <u>737</u>	

Port Point	El. Time, Min.	DGM Reading, 90.4 Ft. 1010	Velocity Head ΔP, in. H ₂ O	Orifice ΔH, in. H ₂ O	Stack Temp. °F	Meter Temp., °F In	Meter Temp., °F Out	Oven Temp. °F	Imp. Temp. °F	Vac. in. Hg
1	000	900.741	1.10	4.20	119	92	88	274	68	3
2	3	906.5	0.62	2.25	120	98	89	268	65	3
3	6	909.0	0.57	2.10	120	103	89	269	62	3
4	9	911.6	0.48	1.80	122	107	90	275	63	7
5	12	913.9	0.45	1.65	123	109	92	272	62	3
6	15	916.2	0.42	1.55	123	111	93	265	60	3
7	18	918.4	0.57	2.10	125	117	94	260	60	3
8	21	921.0	0.40	1.50	122	117	96	231	61	3
9	24	923.3	0.50	1.85	121	117	97	269	62	3
10	27	925.5	0.34	1.25	110	120	99	270	62	3
11										
12										
13	30/00	927.645	0.58	2.15	120	116	99	261	60	3
14	3	930.4	0.53	1.95	124	122	100	269	64	3
15	6	932.8	0.58	2.15	122	123	101	265	64	3
16	9	935.8	0.70	2.60	121	126	103	271	67	4
17	12	938.1	0.69	2.55	120	128	103	268	69	4
18	15	940.8	0.59	2.20	118	129	105	273	65	4
19	18	943.4	0.68	2.55	109	130	106	261	69	4
20	21	946.2	0.66	2.45	108	131	107	274	65	4
21	24	949.2	0.44	1.65	109	131	108	270	66	3
22	27	951.3	0.38	1.40	110	128	108	268	66	3
23	30/30	953.556								
24										
25		2043.043		0.49	006	204	8			
26										
27		2041.041								
28		2039.039								
29										
30		49.546	2318	2.0050	118.30	102.98				
31										
32										
33										

PARTICULATE CATCH ANALYSIS

SAMPLES:

Wayne Farms - Cooler Stock

DATE TAKEN:

9/20/94

DATE ANALYZED:

9/20/94

DELIVERED BY:

Don

RECEIVED BY:

Don

ANALYZED BY:

Don

(Attach chain of custody if additional exchanges occur)

FILTERS:

RUN NO.	1	2	3		
FILTER NO.	2383	2381	2385		
FILTER TARE, gms.	.5657	.5625	.5627		
	.5700	.5653	.5680		
	.5699	.5653	.5683		
FINAL WEIGHT, gms.	.5699	.5653	.5683		
NET GAIN, gms.	.0012	.0028	.0056		

PROBE WASH:

RUN NO.	1	2	3		
CONTAINER I.D.	WFR1	WFR2	WFR3		
VOLUME INTACT?	✓	✓	—		
VOLUME, ml	120	50	120		
TARE WEIGHT, gms.	(A) 104.7116	(E) 99.1360	(84) 105.3511		
	104.7686	99.2376	105.4002		
	104.7684	99.2371	105.4000		
FINAL WEIGHT, gms.	104.7684	99.2371	105.4000		
NET GAIN, gms.	.0568	.1011	.0489		
LESS BLANK, gms.					

PARTICULATE SAMPLE WEIGHT:

RUN NO.	1	2	3		
filter + probe, mg.	61.0	103.9	54.5		

DRY GAS METER CALIBRATION

Meter ID Andersen
 Calibration Method DGM/DGM By DGR
 Calibration Meter ID 651729 Pbar 29.80
 Date 4/11/94

Vac. in. Hg	DH in. H ₂ O	Time min	Calibrating Meter			Field Meter						Y	Q	K	DH _g
			Vi cf	Vf cf	Temp F	Vi cf	Vf cf	Temp. in		Temp. out					
								init	final	init	final				
1	4.00	10.00	348.87	358.001	82	93.507	104.898	100	117	102	103	1.010	1.14	0.71	1.815
1	3.00	11.00	358.001	368.729	84	104.898	115.935	113	129	103	107	1.016	1.01	0.72	1.774
1	2.00	13.00	368.729	379.137	84	115.935	126.714	118	133	107	111	1.020	0.83	0.73	1.738
1	1.00	18.00	379.137	389.442	84	126.714	137.456	118	127	111	115	1.016	0.6	0.74	1.683
1	0.75	20.00	389.442	399.506	84	137.456	148.024	112	125	113	118	1.008	0.53	0.75	1.626
Averages:												1.01			1.73

$$Y = [V_{cal}](P_{bar})(T_{dgm}) / [(V_{dgm})(P_m)(T_{cal})]$$

$$K = Q(\sqrt{(P_m M_m) / ((T_m \text{ out})(DH))})$$

$$Q = ((V_{mi} - V_{mf}) / \text{min.})(T_{M, out} / T_{M, avg})(Y)$$

$$DH@ = 0.921 / K^2$$

Where:

Y = Meter correction factor, dimensionless

V_{cal} = Volume of gas through calibrating meter, cubic feet

V_{dgm} = Volume of gas through field dry gas meter, cubic feet

P_{bar} = Barometric pressure, in. Hg

P_m = Meter pressure, (P_{bar} = DH/13.6)

T_{dgm} = Average dry gas meter temp, degrees R

T_{cal} = Temperature of gas at calibrating meter, degrees R

DRY GAS METER CALIBRATION

Meter ID RAC
 Calibration Method DGM/DGM By WBM
 Calibration Meter ID 651729 Pbar 30.02
 Date 8/30/94

Vac. in. Hg	DH in. H ₂ O	Time min	Calibrating Meter			Field Meter						Y	Q	K	DH@
			Vi ft'	Vf ft'	Temp °F	Vi ft'	Vf ft'	Temp. in		Temp out					
								init.	final	init.	final				
2	2.00	15.00	161.245	173.181	77	501.245	513.049	79	91	78	77	1.014	0.79	0.715	1.802
2	2.00	15.00	173.245	184.785	77	513.049	524.946	97	103	89	79	0.992	0.78	0.695	1.904
2	2.00	15.00	184.785	196.379	77	524.946	536.910	102	108	81	83	0.994	0.78	0.697	1.894
Averages:												1.00			1.87

$$Y = [V_{cal}(P_{bar}(T_{dgm})]/[(V_{dgm})(P_m)(T_{cal})]$$

$$K = Q(\text{sqrt}((P_m M_m)/((T_m \text{ out})(DH)))$$

$$Q = ((V_{mi}-V_{mf})/\text{min.})(T_{M,out}/T_{m,avg})(Y)$$

$$DH@ = 0.921/K^2$$

Where:

Y = Meter correction factor, dimensionless

Vcal = Volume of gas through calibrating meter, cubic feet

Vdgm = Volume of gas through field dry gas meter, cubic feet

Pbar = Barometric pressure, in. Hg

Pm = Meter pressure, (Pbar = DH/13.6)

Tdgm = Average dry gas meter temp, degrees R

Tcal = Temperature of gas at calibrating meter, degrees R

DRY GAS METER CALIBRATION

Meter ID RAC
Calibration Method DGM/DGM **By** DGR
Calibration Meter ID 651729 **Pbar** 29.77
Date 9/20/94

Vac. in. Hg	DH in. H ₂ O	Time min	Calibrating Meter			Field Meter						Y	Q	K	DH@
			V _i ft'	V _f ft'	Temp 'F	V _i ft'	V _f ft'	Temp. in		Temp out					
								init.	final	init.	final				
1	5.00	11.50	199.805	213.726	70	437.242	451.721	104	116	82	87	0.999	1.23	0.696	1.901
1	3.25	12.50	213.726	225.644	70	451.721	464.230	113	112	85	88	0.998	0.98	0.683	1.976
1	2.00	15.00	225.644	236.916	71	464.230	476.105	110	112	88	89	0.996	0.77	0.687	1.952
1	1.50	20.50	236.916	250.473	72	476.105	490.370	110	107	89	89	0.994	0.68	0.697	1.893
1	0.85	21.00	250.473	261.354	72	490.370	501.830	106	104	88	89	0.992	0.53	0.726	1.746
Averages:												1.00			1.89

$$Y = [V_{cal}(P_{bar})(T_{dgm})]/[(V_{dgm})(P_m)(T_{cal})]$$

$$K = Q(\sqrt{(P_m M_m)/((T_m \text{ out})(DH))})$$

$$Q = ((V_{mi} - V_{mf})/\text{min.})(T_{m, \text{out}}/T_{m, \text{avg}})(Y)$$

$$DH@ = 0.921/K^2$$

Where:

Y = Meter correction factor, dimensionless

V_{cal} = Volume of gas through calibrating meter, cubic feet

V_{dgm} = Volume of gas through field dry gas meter, cubic feet

P_{bar} = Barometric pressure, in. Hg

P_m = Meter pressure, (P_{bar} = DH/13.6)

T_{dgm} = Average dry gas meter temp, degrees R

T_{cal} = Temperature of gas at calibrating meter, degrees R