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AP-42 Section Number: 9.9.4

Reference Number: 13

Title: Emission Test Report For Toledo
Alfalfa, Oregon, OH

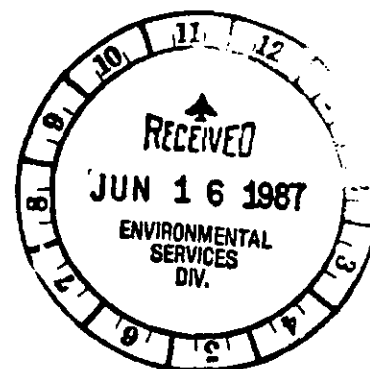
Owens-Illinois Analytical Services

Owens-Illinois Analytical Services

June 1987

AP-42 Section 9.9.4
Reference 13
Report Sect. _____
Reference _____

TOLEDO ALFALFA
COAL FIRED DRYER
EMISSION TEST REPORT
MAY 26, 1987



DATE: June 4, 1987

PROJECT NO.: 03-8069-6254-003

PREPARED BY:

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OWENS-ILLINOIS ANALYTICAL SERVICES

TABLE OF CONTENTS

<u>1.</u>	<u>INTRODUCTION</u>	<u>Page</u>
1.1	Plant Location	1
1.2	Source Tested	1
1.3	Test Date	1
1.4	Testing Organization	1
1.5	Sampling Personnel	1
1.6	Purpose of Tests	1
1.7	Pollutants Measured	1
1.8	Reference Methods Used	1
1.9	Observers Present	1
<u>2.</u>	<u>SUMMARY</u>	
2.1	Emissions	2
2.2	Process Information	2
<u>3.</u>	<u>PROCESS DESCRIPTION</u>	
<u>4.</u>	<u>SAMPLING AND ANALYTICAL PROCEDURES</u>	
4.1	Sampling Location	4
4.2	Velocity Measurements	4
4.3	Particulate	4
4.4	Flue Gas Analysis	5
4.5	Calculations	5
<u>5.</u>	<u>SAMPLE HANDLING AND ASSURANCE PROCEDURES</u>	
5.1	Chain of Custody	6
5.2	Quality Assurance Procedures	6
<u>6.</u>	<u>PROCESS DATA</u>	
6.1	Process Information	7
6.2	Test Results	7
<u>7.</u>	<u>EQUIPMENT CALIBRATION</u>	
7.1	Dry Gas Meter	9
7.2	Pitot Tube	9
7.3	Gravimetric Check	9
7.4	Nozzle	9

TABLE OF CONTENTS
(continued)

TABLE 1 - Process and Emission Summary

LIST OF FIGURES

FIGURE 1 - Schematic of Toledo Alfalfa Dryer &
Cyclone and Traverse Points

FIGURE 2 - Particulate sampling train

FIGURE 3 - EPA Quality Assurance Audits

LIST OF APPENDICES

APPENDIX 1 - Field Data Sheets

APPENDIX 2 - Analytical Results

APPENDIX 3 - Computer Calculations

APPENDIX 4 - Isokinetic Calculations

APPENDIX 5 - Equipment Calibrations

1. INTRODUCTION

1.1 PLANT LOCATION

Toledo Alfalfa Mills, Inc.
861 South Stadium Rd.
Oregon, OH 43616

1.2 SOURCE TESTED

Coal Fired Dryer
Ohio EPA Application 0448020004P001
Permit to Install 04-263

*Triple-pass
dryer*

1.3 TEST DATE

May 26, 1987

1.4 TESTING ORGANIZATION

Owens-Illinois Analytical Services
Environmental Sampling Group
One SeaGate
Toledo, OH 43666
(419) 247-8928

1.5 SAMPLING PERSONNEL

Joseph O. Grau
Paul D. Sagert
Dennis Hiner
Richard Beiswenger

1.6 PURPOSE OF TEST

To document the particulate emissions as requested by
Toledo Environmental Services.

1.7 POLLUTANTS MEASURED

Particulate

1.8 REFERENCE METHODS USED

USEPA Method 1 - Determination of sample points and
cyclonic flow measurement.
USEPA Method 2 - Flue gas velocity measurements.
USEPA Method 3 - Flue gas molecular weight measurement.
USEPA Method 5 - Determination of particulate emissions.

1.9 OBSERVERS PRESENT

Linda Furlough - Toledo Environmental Services
Jeff Twaddle - Toledo Environmental Services

2. SUMMARY

2.1 EMISSIONS

A summary of the emission results is provided below. Additional information is found in Table 1.

<u>Test No.</u>	<u>2</u>	<u>3</u>	<u>4</u>	<u>AVG.</u>
Particulate (lbs/hr.)	28.8	35.7	34.3	32.9

2.2 PROCESS INFORMATION

A summary of the process data is provided below. The operation was running at capacity considering the moisture content of the alfalfa being processed.

Alfalfa Processed (dry) -
Coal Burned -

8,780 lbs/hr.
1,006 lbs/hr.

*10% moisture
load steam ~ 8% moisture
to hammermill
4.39 tons*

NOTE: Test No. 1 was voided due to sampling error.

alfalfa into plant = 60% moisture

3. PROCESS DESCRIPTION

Toledo Alfalfa Mills dries alfalfa in a coal fired rotary dryer. The control equipment consists of the sulfur dioxide sorbant properties of the alfalfa in the drier and a cyclone for particulate removal.

4. SAMPLING AND ANALYTICAL PROCEDURES

4.1 SAMPLING LOCATION

The particulate reference method samples were taken in the cyclone exhaust stack. Cyclonic flow was present and was accounted for in the sampling and velocity measurements. A total of twenty-four (24) traverse points as prescribed in USEPA Method 1 were located on two perpendicular diameters of the stack. A schematic of the cyclone and traverse points can be found in Figure 1.

4.2 VELOCITY MEASUREMENTS

The velocity and angle of the flow were measured at each of the traverse points using an "S" type pitot tube. The procedures detailed in USEPA Methods 1 and 2 were followed. The differential pressures used to calculate the axial components of the flow were calculated by multiplying the measured differential pressures by the squares of the cosines of the angles of the flow with vertical.

4.3 PARTICULATE

4.3.1 Sampling

The Anderson Sampler, Model CU₂ train used is shown schematically in Figure 2. Particulate was collected on the filter and inside surfaces of the probe liner and nozzle. The probe was oriented at each of the traverse points so that the nozzle was pointing directly into the gas stream. The gas stream was sampled isokinetically at each traverse point for times proportional to the cosines of the angles to the flow with the axial direction. The total sampling time was approximately 60 minutes. The sampling train operating parameters monitored during each test are recorded on the field data sheets provided in Appendix 1.

4.3.2 Analytical

Moisture - The moisture was determined from the volume increase of the impingers and silica gel weight gain.

Particulate - The filters were oven dried at 105⁰C for three hours and weighed to 0.1 mg. The acetone probe washes were evaporated at room temperature, dried, cooled, and weighed. The particulate collected was the sum of the weight increase of the filters and the probe wash residue. The Analytical report is provided in Appendix 2.

4.4

FLUE GAS ANALYSIS

The oxygen in the gas stream was measured with a Teledyne Model 320-P Oxygen Analyzer. Carbon dioxide was measured with a Fyrite combustion analyzer.

4.5

CALCULATIONS

The calculations were performed by computer using equations identical to those presented in the EPA reference methods. The printouts are included in Appendix 3. The input data for the velocity head pressure was modified to account for the cyclonic flow. Isokinetic calculations were performed by hand using the time weighed average velocity to account for the non-equal sampling times at the various sample points. These calculations can be found in Appendix 4.

5. SAMPLE HANDLING AND ASSURANCE PROCEDURES

5.1 CHAIN OF CUSTODY

Upon completion of the testing program, the emission samples were hand-carried by the test team to the Owens-Illinois Technical Center in Toledo, Ohio and submitted for subsequent analysis.

5.2 QUALITY ASSURANCE PROCEDURES

Owens-Illinois routinely uses standard methods and techniques combined with appropriate sample blanks in their analysis. Spiked samples are frequently used to insure the precision and accuracy of the analysis.

To further assure the quality of measured data, basic external quality controls, namely Q. A. audits are performed. Results from our most recent EPA Audits for NO_x , SO_2 , CO_2 , CO, and dry gas meter performance are illustrated in Figure 3.

The basic principles, as set forth in Volumes I, II, and III of the Quality Assurance Handbook prepared by the EPA quality Assurance Staff, are used as guidelines in all areas of our environmental testing.

6. PROCESS DATA AND TEST RESULTS

6.1 PROCESS INFORMATION

Process data recorded during the testing is provided on Table 1. There were no upsets or abnormal conditions reported during the testing periods.

6.2 TEST RESULTS

The particulate emissions reported are the total front half catch with the probe and filter maintained at a nominal 250° F. The results are summarized on Table 1 with the detailed computer summaries provided in Appendix 3.

The initial test performed was voided due to improper probe orientation. The computer summary for this test is included in Appendix 3, however the results are not reported.

7. EQUIPMENT CALIBRATION

7.1 DRY GAS METER

The dry gas meter in pump box #1 was calibrated before and after the compliance tests. The volume correction factor (VCF) assigned to the meter is the average of these two calibrations.

Calibration consists of comparing the gas meter being calibrated to a wet test meter in series with the first meter. The wet test meter is calibrated semi-annually by using procedure ASTM D-1071, Section 19.

7.2 PITOT TUBE

The dimensions of pitot tube #22 were measured and are within the tolerances set forth in EPA Method 2 allowing the baseline coefficient of 0.84 to be used.

7.3 GRAVIMETRIC CHECK

Filter weighing was performed with a Mettler H43 balance (#99-28353) located in the Owens-Illinois North Technical Center Building, Toledo, Ohio. The balance is routinely checked by an outside instrument servicing company with NBS standard weights to assure consistent accuracy.

7.4 SAMPLE NOZZLE

The sample nozzle was measured at three equally spaced locations, using vernier calipers in accordance with Method 5. The measurements were recorded on the field data sheets.

All pertinent calibration data sheets are provided in Appendix 5.

TABLE 1
TOLEDO ALFALFA MILLS
PROCESS AND PARTICULATE
EMISSION SUMMARY - MAY 26, 1987

A. GENERAL

1. Test No.	2	3	4	AVG
2. Avg. Gas Temp (⁰ F)	224	224	224	224
3. Avg. Gas Vel.(FPS)	51.9	51.8	51.7	51.8
4. Avg. Gas Vol.(ACFM)	46,811	46,732	46,659	46,734
(DSCFM)	28,842	28,644	29,309	28,932
5. Isokinetic Sample Rate (%)	91	91	96	

B. EMISSIONS

PARTICULATES

(gr/DSCF)	0.117	0.146	0.136	0.133
(lbs./hr)	28.8	35.7	34.3	32.9

C. FLUE GAS ANALYSIS

1. Moisture (%)	18.7	17.9	17.2	17.9
2. Oxygen (%)	17.5	17.5	18	17.7
3. Carbon Dioxide (%)	2.5	3.0	2.5	2.7

D. PROCESS DATA

1. Alfalfa Processed (lbs./hr)	- 8,780 (dry)
2. Coal Usage (lbs./hr)	- 1,006

NOTE: TEST NO. 1 WAS VOIDED DUE TO A SAMPLING ERROR.

FIGURE 1
CYCLONE SCHEMATIC AND
TRAVERSE POINTS

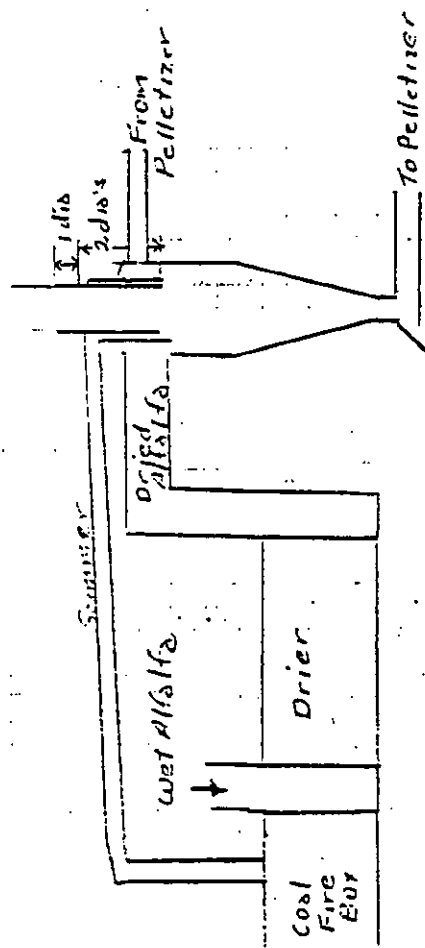
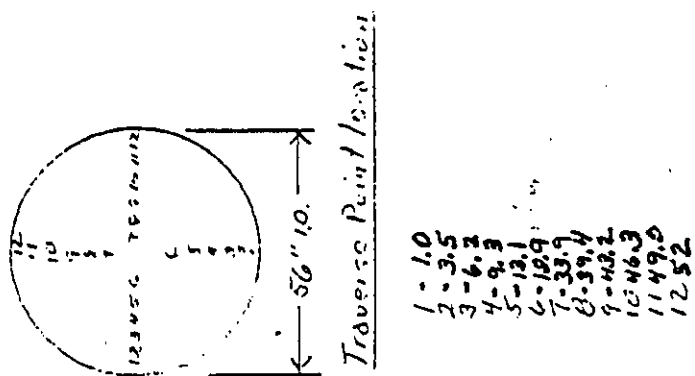


FIGURE 2

PARTICULATE SAMPLING TRAIN

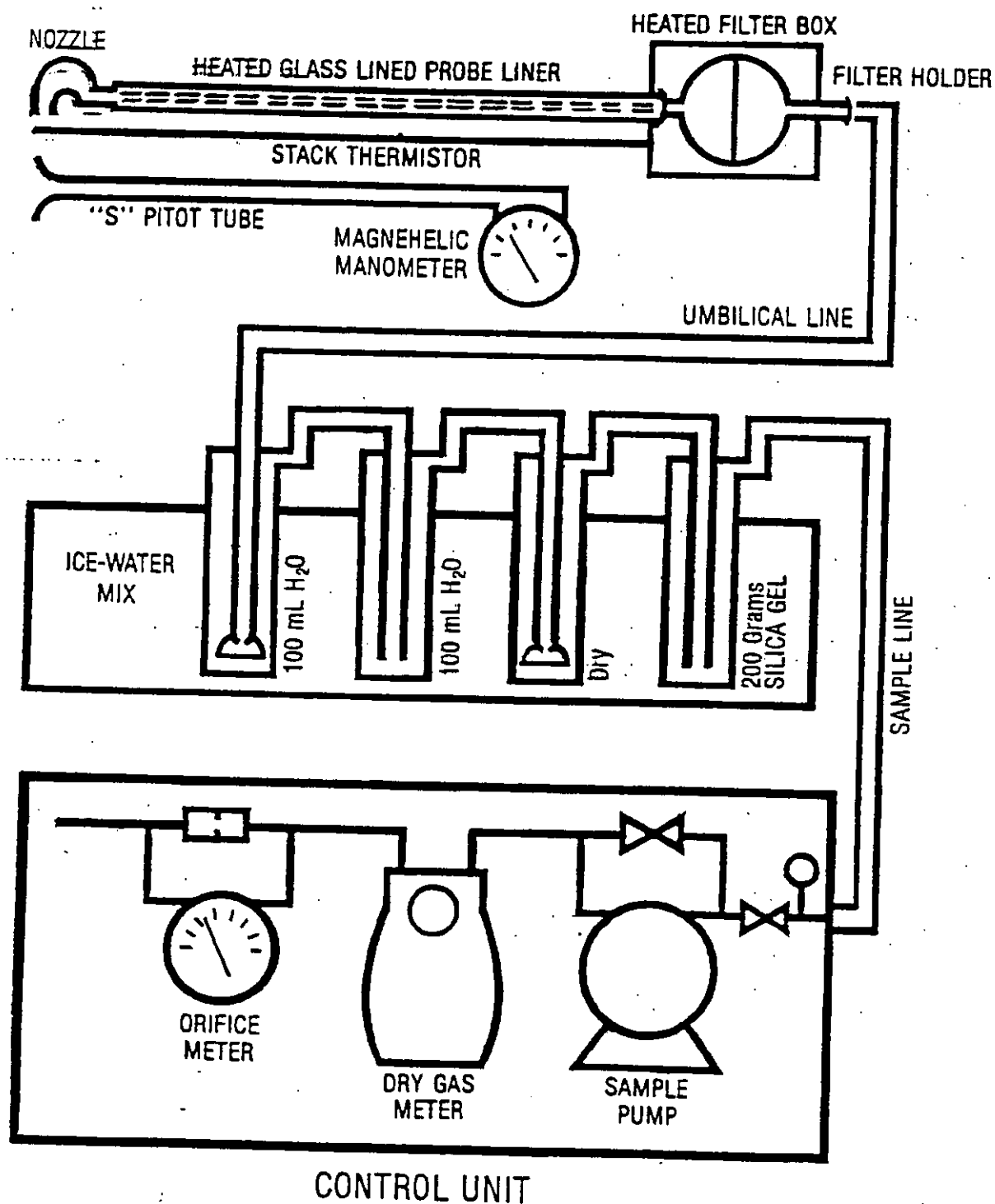
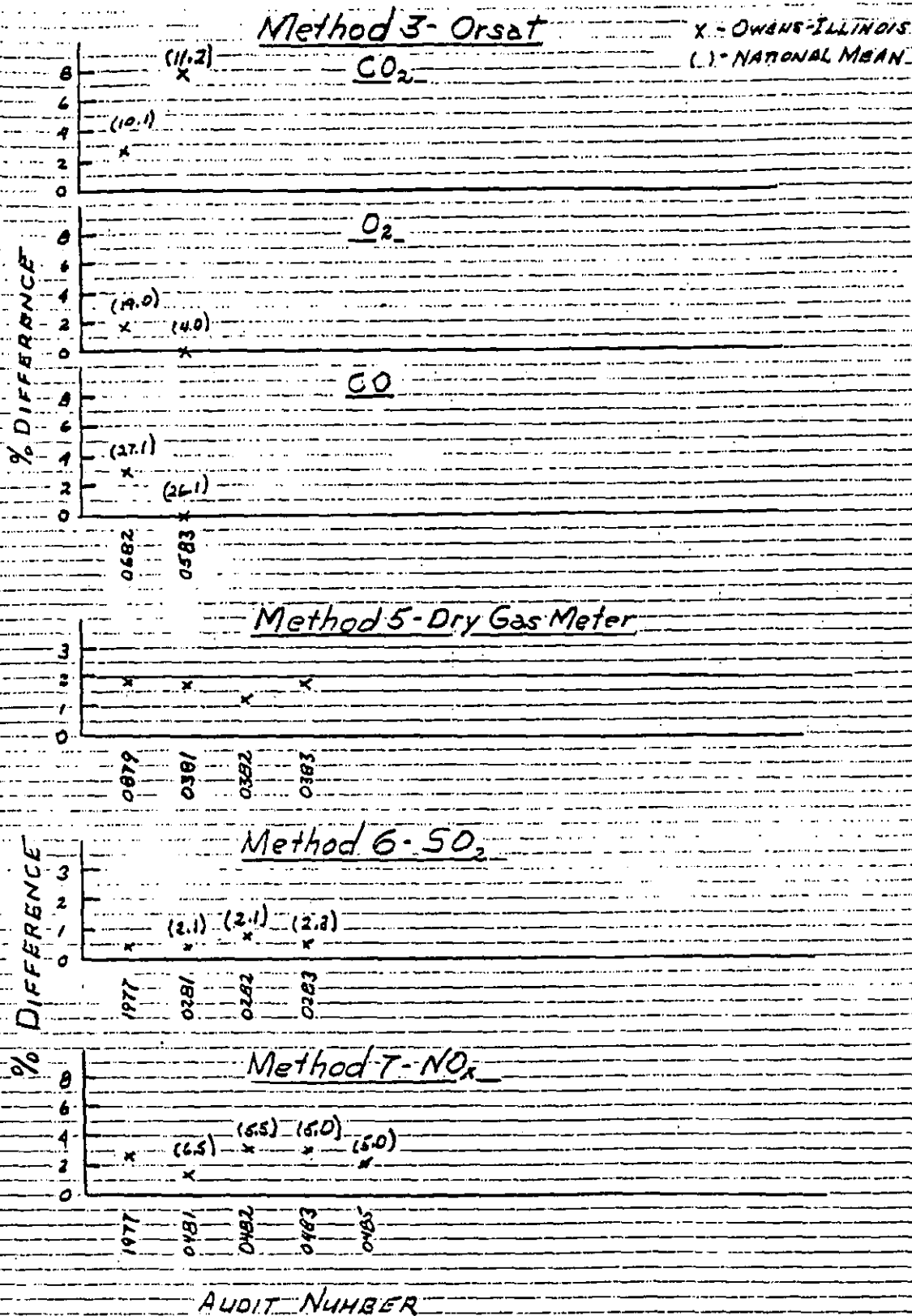


FIGURE 3

EPA QUALITY ASSURANCE AUDITS

APPENDIX 1

FIELD DATA SHEETS

FIELD DATA SHEET

PLANT NO. _____
 LOCATION 70L ALP
 DATE 5-26-87
 TEST NO. 3
 SOURCE 4
 FLUE DIA. 52 1/2 (IN.)
 FLUE AREA _____ (FT²)
 BAROMETRIC PRESS. 29.40
 STATIC PRESS. 0
 PITOT NO. _____ CF
 PUMP BOX NO. _____ VCF
 FILTER WEIGHT _____ (mg)
 PROBE WASH _____ (mg)

NOZZLE DIA. _____ (IN.)
 FLUE GAS: CO _____ (PPM)
 CO₂ _____ (%)
 O₂ _____ (%)
 OTHER _____
 LEAK RATE: BEFORE _____ (SCFM) @ _____ (IN. Hg)
 AFTER _____ (SCFM) @ _____ (IN. Hg)
 WATER VAPOR: CONDENSATE _____ ML
 SILICA GEL _____ ML
 TOTAL _____ ML
 C = _____
 PITOT LEAK CHECK
 POST " " _____

$$\Delta P_c = \frac{C \times (T_p + 460) \times \Delta H_p}{(T_s + 460)}$$

TIME	PT.	DIST. (IN.)	PITOT, ΔH _p (IN. H ₂ O)	STACK, T _s (°F)	METER, V _m CF	VAC. (IN. HG)	PROBE, T _p (°F)	FILTER, T _f (°F)	METER TEMP. (°F)	ORIFICE, ΔP _c (IN. H ₂ O)	ORIFICE, ΔP (IN. H ₂ O)
	0	---	---	---	---	---	---	---	IN OUT	---	---
AP3	1	60	2.9	2.64	32.96		32:58				
1.16	2	50	2.8	3.39	30.32		30:19				
.70	3	60	2.8	2.64	24.93		24:56				
.32	4	70	2.7	1.80	24.29		24:17				
.066	5	80	2.2	0.92	22.19		22:29				
.15	6	70	1.3	1.80	21.57		21:34				
1.77	7	8	1.8	5.27	18.77		18:46				
2.62	8	10	2.7	5.19	14.5		14:30				
0.35	9	70	3.0	1.80	9.31		9:19				
0.61	10	65	3.4	2.23	7.51		7:31				
0.73	11	1.0	2.9	2.64	5.28		5:17				
0.45	12	60	1.8	2.64	2.64		2:38				
AVERAGE											

COMMENTS _____

PERFORMED BY _____

ALF. OBT

FIELD DATA SHEET

PLANT NO. _____
 LOCATION _____
 DATE 5/16/87
 TEST NO. VELTADVERSE
 SOURCE 29.86
 FLUE DIA. 52 1/2 (IN.)
 FLUE AREA 15.03 (FT²)
 BAROMETRIC PRESS. 29.80
 STATIC PRESS. 0" H₂O
 PITOT NO. 22 CF 0.95 X .99
 PUMP BOX NO. _____ VCF _____
 FILTER WEIGHT _____ (mg)
 PROBE WASH _____ (mg)

NOZZLE DIA. _____ (IN.)

FLUE GAS: CO _____ (PPM)

CO₂ _____ (%)O₂ _____ (%)

OTHER _____

LEAK RATE: BEFORE _____ (SCFM) @ _____ (IN. Hg)

AFTER _____ (SCFM) @ _____ (IN. Hg)

WATER VAPOR CONDENSATE _____ ML

SILICA GEL _____ ML

TOTAL _____ ML

PITOT LEAK CHECK

POST " " _____

$$AP_c = \frac{C \times (T_0 + 460) \times 8H_p}{(T_s + 460)}$$

$$2.5 \times 0.95 = 2.375$$

$$2.375 \times 0.99 = 2.351$$

$$2.351 \times 0.99 = 2.327$$

$$2.327 \times 0.99 = 2.304$$

$$2.304 \times 0.99 = 2.281$$

$$2.281 \times 0.99 = 2.258$$

$$2.258 \times 0.99 = 2.235$$

$$2.235 \times 0.99 = 2.212$$

$$2.212 \times 0.99 = 2.189$$

$$2.189 \times 0.99 = 2.166$$

$$2.166 \times 0.99 = 2.143$$

$$2.143 \times 0.99 = 2.120$$

$$2.120 \times 0.99 = 2.097$$

$$2.097 \times 0.99 = 2.074$$

$$2.074 \times 0.99 = 2.051$$

$$2.051 \times 0.99 = 2.028$$

$$2.028 \times 0.99 = 2.005$$

$$2.005 \times 0.99 = 1.982$$

$$1.982 \times 0.99 = 1.959$$

$$1.959 \times 0.99 = 1.936$$

$$1.936 \times 0.99 = 1.913$$

$$1.913 \times 0.99 = 1.890$$

$$1.890 \times 0.99 = 1.867$$

$$1.867 \times 0.99 = 1.844$$

$$1.844 \times 0.99 = 1.821$$

$$1.821 \times 0.99 = 1.798$$

$$1.798 \times 0.99 = 1.775$$

$$1.775 \times 0.99 = 1.752$$

$$1.752 \times 0.99 = 1.729$$

$$1.729 \times 0.99 = 1.706$$

$$1.706 \times 0.99 = 1.683$$

$$1.683 \times 0.99 = 1.660$$

$$1.660 \times 0.99 = 1.637$$

$$1.637 \times 0.99 = 1.614$$

$$1.614 \times 0.99 = 1.591$$

$$1.591 \times 0.99 = 1.568$$

$$1.568 \times 0.99 = 1.545$$

$$1.545 \times 0.99 = 1.522$$

$$1.522 \times 0.99 = 1.499$$

$$1.499 \times 0.99 = 1.476$$

$$1.476 \times 0.99 = 1.453$$

$$1.453 \times 0.99 = 1.430$$

$$1.430 \times 0.99 = 1.407$$

$$1.407 \times 0.99 = 1.384$$

$$1.384 \times 0.99 = 1.361$$

$$1.361 \times 0.99 = 1.338$$

$$1.338 \times 0.99 = 1.315$$

$$1.315 \times 0.99 = 1.292$$

$$1.292 \times 0.99 = 1.269$$

$$1.269 \times 0.99 = 1.246$$

$$1.246 \times 0.99 = 1.223$$

$$1.223 \times 0.99 = 1.200$$

$$1.200 \times 0.99 = 1.177$$

$$1.177 \times 0.99 = 1.154$$

$$1.154 \times 0.99 = 1.131$$

$$1.131 \times 0.99 = 1.108$$

$$1.108 \times 0.99 = 1.085$$

$$1.085 \times 0.99 = 1.062$$

$$1.062 \times 0.99 = 1.039$$

$$1.039 \times 0.99 = 1.016$$

$$1.016 \times 0.99 = 0.993$$

$$0.993 \times 0.99 = 0.970$$

$$0.970 \times 0.99 = 0.947$$

$$0.947 \times 0.99 = 0.924$$

$$0.924 \times 0.99 = 0.901$$

$$0.901 \times 0.99 = 0.878$$

$$0.878 \times 0.99 = 0.855$$

$$0.855 \times 0.99 = 0.832$$

$$0.832 \times 0.99 = 0.809$$

$$0.809 \times 0.99 = 0.786$$

$$0.786 \times 0.99 = 0.763$$

$$0.763 \times 0.99 = 0.740$$

$$0.740 \times 0.99 = 0.717$$

$$0.717 \times 0.99 = 0.694$$

$$0.694 \times 0.99 = 0.671$$

$$0.671 \times 0.99 = 0.648$$

$$0.648 \times 0.99 = 0.625$$

$$0.625 \times 0.99 = 0.602$$

$$0.602 \times 0.99 = 0.579$$

$$0.579 \times 0.99 = 0.556$$

$$0.556 \times 0.99 = 0.533$$

$$0.533 \times 0.99 = 0.510$$

$$0.510 \times 0.99 = 0.487$$

$$0.487 \times 0.99 = 0.464$$

$$0.464 \times 0.99 = 0.441$$

$$0.441 \times 0.99 = 0.418$$

$$0.418 \times 0.99 = 0.395$$

$$0.395 \times 0.99 = 0.372$$

$$0.372 \times 0.99 = 0.349$$

$$0.349 \times 0.99 = 0.326$$

$$0.326 \times 0.99 = 0.303$$

$$0.303 \times 0.99 = 0.280$$

$$0.280 \times 0.99 = 0.257$$

$$0.257 \times 0.99 = 0.234$$

$$0.234 \times 0.99 = 0.211$$

$$0.211 \times 0.99 = 0.188$$

$$0.188 \times 0.99 = 0.165$$

$$0.165 \times 0.99 = 0.142$$

$$0.142 \times 0.99 = 0.119$$

$$0.119 \times 0.99 = 0.096$$

$$0.096 \times 0.99 = 0.073$$

$$0.073 \times 0.99 = 0.050$$

$$0.050 \times 0.99 = 0.027$$

$$0.027 \times 0.99 = 0.004$$

TIME	PT.	DIST. (IN.)	PITOT, AM _p (IN. H ₂ O)	STACK, T _s (°F)	METER, V _m CF #	VAC. (IN. HG)	PROBE, T _p (°F)	FILTER, T _f (°F)	METER TEMP. (°F)	ORIFICE, AP _c (IN. H ₂ O)	ORIFICE, AP (IN. H ₂ O)
		0	---	---		---	---	---	IN OUT	---	---
58		0	---	---		---	---	---			
Ap's		1	50	2.8	3.39	26.99	26.59				
1		2	70	2.8	1.80	23.60	23.36				
0.83		3	55	2.8	3.02	21.80	21.48				
0.92		4	60	2.8	2.64	18.78	18.47				
0.70		5	75	2.4	0.46	16.14	16.08				
0.18		6	75	0.9	1.36	15.68	15.41				
0.54		7	75	2.0	1.36	14.32	14.19				
1.34		8	75	3.1	1.36	12.96	12.58				
0.21		9	70	3.2	1.80	11.60	11.36				
0.87		10	55	2.9	3.02	9.80	9.48				
0.95		11	50	2.8	3.39	6.78	6.47				
1.16		12	50	2.5	3.39	3.39	3.23				
1.103											
AVERAGE											

PERFORMED BY _____

COMMENTS _____

865.3468

1/2

FIELD DATA SHEET

PLANT NO. _____
 LOCATION _____
 DATE 5-26-87
 TEST NO. 1
 SOURCE _____
 FLUE DIA. 52 1/2 IN.
 FLUE AREA (in²)
 BAROMETRIC PRESS. 29.40
 STATIC PRESS. _____
 PITOT NO. 22 CF .05 X .99 1.038
 PUMP BOX NO. 1 VCF 1.032 1.026
 FILTER WEIGHT 201.4 (mg)
 PROBE WASH 78.6 (mg) 2840 mg

TEST
VOIDED

NOZZLE DIA. 3/16 (IN.) .187
 FLUE GAS: CO _____ (PPM) .188
 CO₂ _____ (%) .188
 O₂ _____ (%)
 OTHER _____
 LEAK RATE: BEFORE _____ (SCFM) @ _____ (IN. HG)
 AFTER _____ (SCFM) @ _____ (IN. HG)
 WATER VAPOR: CONDENSATE 182 ML
 SILICA GEL 15 ML
 TOTAL 197 ML
 C = _____
 PITOT LEAK CHECK POST " " _____

$$AP_c = \frac{C \times (T_0 + 460) \times \Delta H_p}{(T_s + 460)}$$

NE Port

TIME	PT.	DIST. (IN.)	PITOT, ΔH_p (IN. H ₂ O)	STACK, T _s (°F)	METER, V _m CF @	VAC. (IN. HG)	PROBE, T _p (°F)	FILTER, T _f (°F)	METER TEMP. (°F)	ORIFICE, ΔP_c (IN. H ₂ O)	ORIFICE, ΔP (IN. H ₂ O)
	0	---	---	---	6242.385	---	---	---	IN OUT	---	---
1.37	1		1.8	230	6244.3	---	250	220	97	0.44	
5.14	2		2.9	220	6246.6	1	240	210	102	0.72	
7.59	3		3.4	220	6248.0	1	250	210	103	0.86	
10.49	4		3.0	220	6250.3		280	200	103	0.76	
11.20	5		2.7	210	---		230	200	104	0.69	
11.27	6		1.8	210	---		270	200	107	0.46	
14.17	7		1.3	210	6254.2		250	190	110	0.34	
17.16	8		2.2	220	6256.8		230	175	111	0.56	
20.07	9		2.7	220	6258.1		250	170	113	0.69	
22.44	10		2.8	220	6259.5		220	180	115	0.72	
25.03	11		2.8	230	6261.6		280	220	120	0.73	
27.40	12		2.9	230	6263.77		270	270	123	0.75	
AVERAGE					44.29				122.0	0.66	

COMMENTS _____

PERFORMED BY _____

IAT
TES

2 of 2

FIELD DATA SHEET

PLANT NO. Toledo HIFALFA

LOCATION _____

DATE 5/26/87

TEST NO. 1

SOURCE _____

FLUE DIA. _____ (IN.)

FLUE AREA _____ (FT²)

BAROMETRIC PRESS. _____

STATIC PRESS. _____

PITOT NO. _____ CF _____

PUMP BOX NO. _____ VCF _____

FILTER WEIGHT _____ (mg)

PROBE WASH _____ (mg)

NOZZLE DIA. 3/16 (IN.)

FLUE GAS: CO _____ (PPM)

CO₂ 2.5 (%)

O₂ 17.5 (%)

OTHER _____

LEAK RATE: BEFORE 0.005 (SCFM) @ 15 (IN. HG)

AFTER 0.005 (SCFM) @ 15 (IN. HG)

WATER VAPOR: CONDENSATE 182 ML

SILICA GEL _____ ML

TOTAL _____ ML

C = 0.305

PITOT LEAK CHECK _____

$$\Delta P_c = \frac{C \times (T_0 + 460) \times \Delta H}{(T_s + 460)}$$

PAST " " " "

SE Port

TIME	PT.	DIST. (IN.)	PITOT, ΔH _D (IN. H ₂ O)	STACK, T _S (°F)	METER, V _m CF @	VAC. (IN. HG)	PROBE, T _p (°F)	FILTER, T _f (°F)	METER TEMP. (°F)	ORIFICE, ΔP _C (IN. H ₂ O)	ORIFICE, ΔP (IN. H ₂ O)
	0				6263.770				IN OUT		
2.19	1		2.5	230		1	250	290	127 125	0.65	
4.38	2		2.8	230	6267.25		210	290	128 126	0.73	
7.07	3		2.9	225	6269.2		255	275	130 127	0.76	
9.58	4		3.2	230	6271.65		280	260	131 128	0.84	
12.53	5		3.1	230	6274.0		260	240	134 130	0.81	
15.48	6		2.0	230	6275.9		250	230	135 130	0.52	
18.43	7		0.8	225	6277.25		235	230	136 131	0.21	
21.44	8		2.4	220	6280.6	2	230	240	137 132	0.64	
24.42	9		2.8	225	6281.5	2	255	250	138 134	0.74	
26.50	10		2.8	225	6283.3	1	170	270	140 135	0.74	
29.40	11		2.8	230	6286.7	1	270	270	137 135	0.74	
31.59	12			220	6286.570	1	270	270	138 136	0.75	
AVERAGE											

COMMENTS _____

PERFORMED BY _____

JM
TES

182

PROBE WASH 120.9 (mg)

$$\Delta P_C = \frac{C \times (T_0 + 460) \times \Delta H}{(T_c + 460)}$$

NE Port

TIME	PT.	DIST. (IN.)	PITOT, h_p (IN. H_2O)	STACK, T_s (°F)	METER, V_m CF @	VAC. (IN. HG)	PROBE, T_p (°F)	FILTER, T_f (°F)	METER TEMP. (°F)	ORIFICE, ΔP_c (IN. H_2O)	ORIFICE, ΔP (IN. H_2O)
	0	---	---	---	6288.022	---	---	---	IN OUT	---	---
2:38	1		1.8	220	6289.7	---	260	210	112 112	0.49	
5:17	2		2.9	220	6291.8	---	240	280	115 114	0.79	
7:31	3		3.4	220	6293.8	1	270	315	117 117	0.93	
9:19	4		3.0	220	6295.3	1	265	300	121 118	0.82	
14:30	5		2.7	220	6299.3	1	245	270	122 118	0.74	
19:46	6		1.8	220	6302.65	1	235	235	125 120	0.49	
21:34	7		1.3	220	6303.68	1	280	210	127 121	0.36	
22:29	8		2.2	220	6304.3	2	240	220	127 122	0.61	
24:17	9		2.7	230	6305.75	2	230	225	127 122	0.74	
26:56	10		2.8	230	6307.8	2	250	235	128 122	0.76	
30:14	11		2.8	230	6310.6	1	220	240	130 123	0.76	
32:54	12		2.9	240	6312.718	1	280	250	131 125	0.78	
AVERAGE					45.47				127.6	0.70	

COMMENTS

PERFORMED BY

STAT
TES

FIELD DATA SHEET

PLANT NO. Toledo Alfalfa

LOCATION _____

DATE 5/26/87

TEST NO. 2

SOURCE _____

FLUE DIA. _____ (IN.)

FLUE AREA _____ (FT²)

BAROMETRIC PRESS. _____

STATIC PRESS. _____

PITOT NO. _____ CF _____

PUMP BOX NO. _____ VCF _____

FILTER WEIGHT _____ (mg)

PROBE WASH _____ (mg)

NOZZLE DIA. _____ (IN.)

FLUE GAS: CO _____ (PPM)

CO₂ _____ (%)

O₂ _____ (%)

OTHER _____

LEAK RATE: BEFORE 0.005 (SCFM) @ 8 (IN. HG)

AFTER 0.01 (SCFM) @ 10 (IN. HG)

WATER VAPOR: CONDENSATE _____ ML

SILICA GEL _____ ML

TOTAL _____ ML

C = _____ PITOT LEAK CHECK _____

PAST " " " "

$$\Delta P_C = \frac{C \times (T_0 + 460) \times \Delta M_p}{(T_s + 460)}$$

SE Port

TIME	PT.	DIST. (IN.)	PITOT, ΔM _p (IN. H ₂ O)	STACK, T _s (°F)	METER, V _m CF @	VAC. (IN. HG)	PROBE, T _p (°F)	FILTER, T _f (°F)	METER TEMP. (°F)	ORIFICE, ΔP _C (IN. H ₂ O)	ORIFICE, ΔP (IN. H ₂ O)
	0	---	---	---	6312.719	---	---	---	IN OUT	---	---
3:23	1		2.5	220	6315.3	1	230	240	133 128	0.69	
6:47	2		2.8	230	6318.0	1	260	230	133 129	0.77	
9:48	3		2.9	230	6320.5	1	240	230	133 129	0.80	
11:36	4		3.2	230	6322.0	1	230	240	135 130	0.88	
12:58	5		3.1	230	6323.15	2	260	260	136 130	0.85	
14:19	6		2.0	230	6324.35	2	270	275	137 130	0.55	
15:41	7		0.8	220	6325.4		250	260	137 130	0.22	
16:01	8		2.4	220	6326.8	2	240	270	138 131	0.67	
18:47	9		2.8	220	6327.8	1	280	250	139 132	0.78	
21:48	10		2.8	230	6330.4	1	260	240	140 132	0.77	
23:36	11		2.8	230	6331.7	1	250	230	141 133	0.77	
26:59	12		2.8	220	6333.489		240	230	141 135	0.79	
AVERAGE											

COMMENTS _____

PERFORMED BY _____

SWT
TES

FIELD DATA SHEET

PLANT NO. Toledo Affn/4
 LOCATION _____
 DATE 5/26/87
 TEST NO. 3
 SOURCE _____
 FLUE DIA. _____ (IN.)
 FLUE AREA _____ (FT²)
 BAROMETRIC PRESS. _____
 STATIC PRESS. _____
 PITOT NO. _____ CF .84
 PUMP BOX NO. 1 VCF _____
 FILTER WEIGHT 232.8 (mg)
 PROBE WASH 157.0 (mg) 389.8

NOZZLE DIA. 3/16 (IN.)
 FLUE GAS: CO _____ (PPM)
 CO₂ 3 (%)
 O₂ 17 1/2 (%)
 OTHER _____
 LEAK RATE: BEFORE _____ (SCFM) @ _____ (IN. HG)
 AFTER _____ (SCFM) @ _____ (IN. HG)
 WATER VAPOR: CONDENSATE 183 ML
 SILICA GEL 11.5 ML
 TOTAL 194.5 ML
 C = _____ PITOT LEAK CHECK _____

$$\Delta P_c = \frac{C \times (T_0 + 460) \times \Delta H}{(T_s + 460)}$$

NE Port

TIME	PT.	DIST. (IN.)	PITOT, ΔH _p (IN. H ₂ O)	STACK, T _s (°F)	METER, V _m CF @	VAC. (IN. HG)	PROBE, T _p (°F)	FILTER, T _f (°F)	METER TEMP. (°F)	ORIFICE, ΔP _c (IN. H ₂ O)	ORIFICE, ΔP (IN. H ₂ O)
	0	---	---	---	6334.581	---	---	---	IN OUT	---	---
2:38	1		1.8	220	6336.2	2	240	290	127 128	0.50	
5:17	2		2.9	230	6338.55	3	270	290	125 127	0.79	
7:31	3		3.4	230	6340.6		240	290	125 125	0.93	
9:19	4		3.0	220	6342.05	2	280	275	128 126	0.82	
14:30	5		2.7	220	6346.2	3	270	240	128 126	0.75	
19:46	6		1.8	230	6349.65	2	240	230	130 127	0.49	
21:34	7		1.3	220	6350.6		250	230	131 127	0.36	
22:29	8		2.2	220	6351.3		230	230	132 128	0.61	
24:17	9		2.7	220	6352.7	2	250	230	132 129	0.75	
26:56	10		2.8	220	6354.8	2 1/2	240	240	135 130	0.78	
30:19	11		2.8	230	6356.55	2	250	250	135 130	0.77	
32:58	12		2.9	220	6359.762	2	270	260	137 131	0.81	
AVERAGE					46.51				134.7	0.71	

COMMENTS _____

PERFORMED BY _____

JAT
TKS

FIELD DATA SHEET

PLANT NO. Toledo Alfalfa

LOCATION _____

DATE 5/26/87

TEST NO. 3

SOURCE _____

FLUE DIA. _____ (IN.)

FLUE AREA _____ (FT²)

BAROMETRIC PRESS. _____

STATIC PRESS. _____

PITOT NO. _____ CF _____

PUMP BOX NO. _____ VCF _____

FILTER WEIGHT _____ (mg)

PROBE WASH _____ (mg)

NOZZLE DIA. _____ (IN.)

FLUE GAS: CO _____ (PPM)

CO₂ _____ (%)

O₂ _____ (%)

OTHER _____

LEAK RATE: BEFORE 0.005 (SCFM) @ 11 (IN. HG)

AFTER 0.005 (SCFM) @ 10 (IN. HG)

WATER VAPOR: CONDENSATE +183 ML

SILICA GEL _____ ML

TOTAL _____ ML

C = _____ PITOT LEAK CHECK _____
 " " " " " "

$$\Delta P_c = \frac{C \times (T_0 + 460) \times \Delta H_p}{(T_s + 460)}$$

SE Port

TIME	PT.	DIST. (IN.)	PITOT, ΔH _p (IN. H ₂ O)	STACK, T _s (°F)	METER, V _m CF @	VAC. (IN. HG)	PROBE, T _p (°F)	FILTER, T _f (°F)	METER TEMP. (°F)	ORIFICE, ΔP _c (IN. H ₂ O)	ORIFICE, ΔP (IN. H ₂ O)
	0	—	—	—	6359.762	—	—	—	IN / OUT	—	—
3:23	1		2.5	220	6362.4	2	250	290	131 / 132	0.70	
6:47	2		2.8	220	6365.15	2	240	320	139 / 134	0.79	
9:48	3		2.9	220	6367.75	2 1/2	230	290	141 / 135	0.82	
11:36	4		3.2	220	6369.25	3	260	280	142 / 136	0.90	
12:58	5		3.1	220	6370.41	3	240	270	144 / 137	0.87	
14:19	6		2.0	220	6371.4	2	230	260	145 / 138	0.57	
15:41	7		0.8	220	6372.05	1	260	250	146 / 139	0.23	
16:08	8		2.4	220	—		240	240	146 / 139	0.68	
18:47	9		2.8	220	6374.4		225	220	145 / 140	0.79	
21:48	10		2.8	220	6376.86		260	210	146 / 140	0.79	
22:36	11		2.8	220	6378.4	2 1/2	230	180	147 / 140	0.79	
26:59	12		2.8	220	6381.093	2 1/2	220	200	146 / 140	0.79	
AVERAGE											

COMMENTS _____

PERFORMED BY _____

Handwritten signature/initials
 TES

FIELD DATA SHEET

PLANT NO. Toledo Alfa4

LOCATION _____

DATE 5/26/87

TEST NO. 4

SOURCE _____

FLUE DIA. _____ (IN.)

FLUE AREA _____ (FT²)

BAROMETRIC PRESS. _____

STATIC PRESS. _____

PITOT NO. _____ CF PH

PUMP BOX NO. 1 VCF 1.032

FILTER WEIGHT 261.4 (mg)

PROBE WASH 125.2 (mg)

NOZZLE DIA. 3/16 (IN.)

FLUE GAS: CO _____ (PPM)

CO₂ 24 (%)

O₂ 18 (%)

OTHER _____

LEAK RATE: BEFORE _____ (SCFM) @ _____ (IN. HG)

AFTER _____ (SCFM) @ _____ (IN. HG)

WATER VAPOR: CONDENSATE 182 ML

SILICA GEL 10.4 ML

TOTAL 192.4 ML

C = _____ PITOT LEAK CHECK _____

$$AP_c = \frac{C \times (T_0 + 460) \times \Delta H}{(T_s + 460)}$$

NE Port

TIME	PT.	DIST. (IN.)	PITOT, ΔH_p (IN. H ₂ O)	STACK, T_s (°F)	METER, V_m CF #	VAC. (IN. HG)	PROBE, T_p (°F)	FILTER, T_f (°F)	METER TEMP. (°F)	ORIFICE, ΔP_c (IN. H ₂ O)	ORIFICE, ΔP (IN. H ₂ O)
	0	---	---	---	6381.222	---	---	---	IN OUT	---	---
2:38	1		1.8	230	6383.35	---	250	200	125 125	0.49	
5:17	2		2.9	230	6385.7	---	240	260	125 125	0.79	
7:31	3		3.4	235	6387.35	1	220	300	125 123	0.92	
9:19	4		3.0	230	6389.83	1	250	310	125 123	0.81	
11:30	5		2.7	230	6393.05	1	215	275	127 124	0.73	
14:46	6		1.8	230	6396.5	---	235	250	127 123	0.49	
21:34	7		1.3	220	6397.55	---	240	250	128 123	0.36	
22:29	8		2.2	220	6398.1		210	240	127 123	0.61	
24:17	9		2.7	220	6399.55		240	235	128 123	0.74	
26:52	10		2.8	220	6401.7	1	265	235	129 123	0.77	
30:19	11		2.8	220	6404.4	1	230	250	129 123	0.77	
32:58	12		2.9	220	6406.604	1	250	255	129 123	0.80	
AVERAGE					47.69				124.8	0.70	

COMMENTS _____

PERFORMED BY _____

JAT
TES

FIELD DATA SHEET

PLANT NO. Toledo Alfalfa

LOCATION _____

DATE 5/26/87

TEST NO. A

SOURCE _____

FLUE DIA. _____ (IN.)

FLUE AREA _____ (FT²)

BAROMETRIC PRESS. _____

STATIC PRESS. _____

PITOT NO. _____ CF _____

PUMP BOX NO. _____ VCF _____

FILTER WEIGHT _____ (mg)

PROBE WASH _____ (mg)

NOZZLE DIA. _____ (IN.)

FLUE GAS: CO _____ (PPM)

CO₂ _____ (%)

O₂ _____ (%)

OTHER _____

LEAK RATE: BEFORE 0.002 (SCFM) @ 11 (IN. Hg)

AFTER 0.000 (SCFM) @ 10 (IN. Hg)

WATER VAPOR: CONDENSATE _____ ML

SILICA GEL _____ ML

TOTAL _____ ML

C = _____ PITOT LEAK CHECK _____
 " " " " " "

$$AP_c = \frac{C \times (T_0 + 460) \times \Delta P_0}{(T_s + 460)}$$

SE
Port

page 2 of 2

TIME	PT.	DIST. (IN.)	PITOT, Δh_p (IN. H ₂ O)	STACK, T_s (°F)	METER, V_m CF @	VAC. (IN. HG)	PROBE, T_p (°F)	FILTER, T_f (°F)	METER TEMP. (°F)	ORIFICE, ΔP_c (IN. H ₂ O)	ORIFICE, ΔP (IN. H ₂ O)
	D	—	—	—	6406.604	—	—	—	IN OUT	—	—
3:23	1		2.5	220	6409.24	—	270	280	127 123	0.69	
6:47	2		2.5	220	6412.9		240	265	128 123	0.77	
9:48	3		2.9	220	6414.6		250	250	127 123	0.80	
11:36	4		3.2	220	6416.2		220	250	129 123	0.88	0.88
12:58	5		3.1	220	6417.9		250	250	129 123	0.85	
14:19	6		2.0	220	6419.5		220	260	130 123	0.55	
15:41	7		0.8	220	6422.5				130 123	0.22	
16:08	8		2.4	—							
18:47	9		2.8								
21:48	10		2.8								
23:36	11		2.8								
26:59	12		2.8								
AVERAGE											

COMMENTS _____

PERFORMED BY _____

JH
TES

FIELD DATA SHEET

PLANT NO. Toledo Alfalfa

LOCATION _____

DATE 5/26/87

TEST NO. 4

SOURCE _____

FLUE DIA. _____ (IN.)

FLUE AREA _____ (FT²)

BAROMETRIC PRESS. _____

STATIC PRESS. _____

PITOT NO. _____ CF

PUMP BOX NO. _____ VCF

FILTER WEIGHT _____ (mg)

PROBE WASH _____ (mg)

NOZZLE DIA. _____ (IN.)

FLUE GAS: CO _____ (PPM)

CO₂ _____ (%)

O₂ _____ (%)

OTHER _____

LEAK RATE: BEFORE _____ (SCFM) @ _____ (IN. HG)

AFTER _____ (SCFM) @ _____ (IN. HG)

WATER VAPOR CONDENSATE _____ ML

SILICA GEL _____ ML

TOTAL _____ ML

C = _____ PITOT LEAK CHECK _____
Past " " "

$$\Delta P_c = \frac{C \times (T_0 + 460) \times \Delta H_D}{(T_s + 460)}$$

TIME	PT.	DIST. (IN.)	PITOT, ΔH _D (IN. H ₂ O)	STACK, T _s (°F)	METER, V _m CF #	VAC. (IN. HG)	PROBE, T _p (°F)	FILTER, T _f (°F)	METER TEMP. (°F)	ORIFICE, ΔP _c (IN. H ₂ O)	ORIFICE, ΔP (IN. H ₂ O)
	0	---	---	---		---	---	---	IN OUT	---	---
	1										
	2										
	3										
	4										
	5										
	6										
15:44	7		6.8	220	6420.5				130 124	0.22	
16:08	8		2.4	220	6421.1		230	240	123 121	0.77	
18:47	9		2.8	220	6422.55		250	255	123 121	0.62	
21:41	10		2.8	220	6424.8	1	230	240	123 121	0.77	
23:30	11		2.8	220	6426.6	1	270	220	123 121	0.77	
26:59	12		2.8	220	6428.910	1	250	230	126 121	0.77	
AVERAGE											

COMMENTS _____

PERFORMED BY _____

JHT
TES

APPENDIX 2

ANALYTICAL DATA

DATE RECEIVED 5/27/87
DATE COMPLETED 5/29/87

TOLEDO ALFALFA MILLS
GRAVIMETRIC ANALYSIS

FILTERS: Oven dried 105⁰C for three hours and weighed.

<u>TEST NO.</u>	<u>TARE WT. (Grams)</u>	<u>DRY WT. (Grams)</u>	<u>PATRICULATE (Grams)</u>
1 *	0.8082	1.0096	0.2014
2	0.7963	0.9888	0.1925
3	0.8034	1.0362	0.2328
4	0.8000	1.0614	0.2614
Blank	0.8010	0.8010	0.0000

ACETONE PROBE WASHES:

Transferred to platinum weighing dishes evaporated in air,
oven dried 105⁰C/3 hours, cooled in desiclator, weighed.
One hour cycles to constant weight.

<u>TEST NO.</u>	<u>TARE WT. (Grams)</u>	<u>DRY WT. (Grams)</u>	<u>PATRICULATE (Grams)</u>
1 *	91.4222	91.5008	0.0786
2	93.3362	93.4571	0.1209
3	92.2610	92.4180	0.1570
4	90.7843	90.9095	0.1252
Blank	94.9590	94.9595	0.0005

*Results shown but not included, Test #1 was voided.

APPENDIX 3

COMPUTER CALCULATIONS

OWENS ILLINOIS, INC.

TEST
VOIDED

PLANT: TOLEDO ALFALFA MILLS
 DATE: 5-26-87
 UNIT TESTED: TEST #1

	VH(IN H2O)	TS(K)	TS(F)	VS(MPS)	VS(FPS)
1	0.730	383.	230.	17.4	57.2
2	1.160	383.	230.	22.0	72.0
3	0.700	377.	220.	16.9	55.6
4	0.320	377.	220.	11.5	37.6
5	0.660	377.	220.	16.4	54.0
6	0.150	372.	210.	7.8	25.5
7	1.770	372.	210.	26.7	87.7
8	2.620	372.	210.	32.5	106.7
9	0.350	377.	220.	12.0	39.3
10	0.610	377.	220.	15.8	51.9
11	0.730	377.	220.	17.3	56.7
12	0.450	383.	230.	13.7	44.9
13	1.160	383.	230.	22.0	72.0
14	0.330	380.	225.	11.7	38.3
15	0.920	380.	225.	19.5	63.9
16	0.700	380.	225.	17.0	55.8
17	0.018	383.	230.	2.7	9.0
18	0.054	383.	230.	4.7	15.5
19	0.134	383.	230.	7.5	24.5
20	0.210	383.	230.	9.3	30.7
21	0.370	380.	225.	12.4	40.5
22	0.950	383.	230.	19.9	65.2
23	1.160	383.	230.	22.0	72.0
24	1.030	383.	230.	20.7	67.9
AVERAGE		380.	224.	15.8	51.9

PS = 747.	MMHG (29.40 INHG)	CP = 0.840
DS = 1.33 M	(52.5 IN)	VCF = 1.032
A = 1.40 SQM	(15.03 SQFT)	DH = 1.
%CO2 = 2.5		MMHG (0.7 INH2O)
%CO = 0.0		PB = 747.
%O2 = 17.5		MMHG (29.40 INHG)
%N2 = 80.0		TM = 50.
		C (122.0 F)
		WC = 197.
		ML
		VMC = 1.254 CUM (44.290 CUFT)
		VSTD = 1.156 CUM (40.81 CUFT)
ST = 60. MIN		DN = 4.78 MM (0.188 IN)
MD = 29.10		MS = 27.04

MG COLLECTED

PARTICULATES

280.0

OWENS ILLINOIS, INC.

TEST
VOIDED

PLANT: TOLEDO ALFALFA MILLS
DATE: 5-26-87
UNIT TESTED: TEST #1

	CONCENTRATION		EMISSION RATE	
	G/DSCM	GR/DSCF	G/SEC	LB/HR
PARTICULATES	0.243	0.106	3.30	26.2

FLUE GAS VOLUME 22.08 ACMS (46789.ACFM)
 13.64 DSCMS(28908.DSCFM)

MOISTURE 18.51%

STANDARD CONDITIONS- 68.F, 29.92INHG

OWENS ILLINOIS, INC.

PLANT: TOLEDO ALFALFA MILLS
 DATE: 5-26-87
 UNIT TESTED: TEST #2

	VH(IN H2O)	TS(K)	TS(F)	VS(MPS)	VS(FPS)
1	0.730	383.	230.	17.4	57.2
2	1.160	383.	230.	22.0	72.1
3	0.700	377.	220.	16.9	55.6
4	0.320	377.	220.	11.5	37.6
5	0.660	377.	220.	16.5	54.0
6	0.150	372.	210.	7.8	25.5
7	1.770	372.	210.	26.7	87.7
8	2.620	372.	210.	32.5	106.7
9	0.350	377.	220.	12.0	39.3
10	0.610	377.	220.	15.8	51.9
11	0.730	377.	220.	17.3	56.8
12	0.450	383.	230.	13.7	44.9
13	1.160	383.	230.	22.0	72.1
14	0.330	380.	225.	11.7	38.3
15	0.920	380.	225.	19.5	64.0
16	0.700	380.	225.	17.0	55.8
17	0.018	383.	230.	2.7	9.0
18	0.054	383.	230.	4.7	15.6
19	0.134	383.	230.	7.5	24.5
20	0.210	383.	230.	9.3	30.7
21	0.370	380.	225.	12.4	40.6
22	0.950	383.	230.	19.9	65.2
23	1.160	383.	230.	22.0	72.1
24	1.030	383.	230.	20.7	67.9
AVERAGE		380.	224.	15.8	51.9

PS = 747.	MMHG (29.40 INHG)	CP = 0.840
DS = 1.33 M	(52.5 IN)	VCF = 1.032
A = 1.40 SQM	(15.03 SQFT)	DH = 1.
%CO2 = 2.5		MMHG (0.7 INH2O)
%CO = 0.0		PB = 747.
%O2 = 17.5		TM = 53.
%N2 = 80.0		C (127.6 F)
		WC = 203.
		ML
ST = 60.	MIN	VMC = 1.288 CUM (45.470 CUFT)
MD = 29.10		VSTD = 1.175 CUM (41.51 CUFT)
		DN = 4.78 MM (0.188 IN)
		MS = 27.02

MG COLLECTED

PARTICULATES

313.4

OWENS ILLINOIS, INC.

PLANT: TOLEDO ALFALFA MILLS
DATE: 5-26-87
UNIT TESTED: TEST #2

	CONCENTRATION		EMISSION RATE	
	G/DSCM	GR/DSCF	G/SEC	LB/HR
PARTICULATES	0.267	0.117	3.63	28.8
FLUE GAS VOLUME	22.09 ACMS (46811.ACFM)			
	13.61 DSCMS(28842.DSCFM)			
MOISTURE	18.74%			

STANDARD CONDITIONS- 68.F, 29.92INHG

OWENS ILLINOIS, INC.

PLANT: TOLEDO ALFALFA MILLS
DATE: 5-26-87
UNIT TESTED: TEST #3

	VH(IN H2O)	TS(K)	TS(F)	VS(MPS)	VS(FPS)
1	0.730	383.	230.	17.4	57.1
2	1.160	383.	230.	21.9	72.0
3	0.700	377.	220.	16.9	55.5
4	0.320	377.	220.	11.4	37.5
5	0.660	377.	220.	16.4	53.9
6	0.150	372.	210.	7.9	25.5
7	1.770	372.	210.	26.7	87.6
8	2.620	372.	210.	32.5	106.6
9	0.350	377.	220.	12.0	39.2
10	0.610	377.	220.	15.8	51.8
11	0.730	377.	220.	17.3	56.7
12	0.450	383.	230.	13.7	44.8
13	1.160	383.	230.	21.9	72.0
14	0.330	380.	225.	11.7	38.2
15	0.920	380.	225.	19.5	63.9
16	0.700	380.	225.	17.0	55.7
17	0.018	383.	230.	2.7	9.0
18	0.054	383.	230.	4.7	15.5
19	0.134	383.	230.	7.5	24.5
20	0.210	383.	230.	9.3	30.6
21	0.370	380.	225.	12.3	40.5
22	0.950	383.	230.	19.8	65.1
23	1.160	383.	230.	21.9	72.0
24	1.030	383.	230.	20.7	67.9
AVERAGE		380.	224.	15.8	51.8

PS = 747.	MMHG (29.40 INHG)	CP = 0.840
DS = 1.33 M	(52.5 IN)	VCF = 1.032
A = 1.40 SQM	(15.03 SQFT)	DH = 1.
%CO2 = 2.5		MMHG (0.7 INH2O)
%CO = 0.0		PB = 747.
%O2 = 17.5		MMHG (29.40 INHG)
%N2 = 80.0		TM = 57.
		C (134.7 F)
		WC = 195.
		ML
		VMC = 1.317 CUM (46.510 CUFT)
		VSTD = 1.170 CUM (41.31 CUFT)
ST = 60. MIN		DN = 4.78 MM (0.188 IN)
MD = 29.10		MS = 27.11

MG COLLECTED

PARTICULATES

389.8

OWENS ILLINOIS, INC.

PLANT: TOLEDO ALFALFA MILLS
DATE: 5-26-67
UNIT TESTED: TEST #3

	CONCENTRATION		EMISSION RATE	
	G/DSCM	GR/DSCF	G/SEC	LB/HR
PARTICULATES	0.334	0.146	4.50	35.7
FLUE GAS VOLUME	22.06 ACMS (46732.ACFM)			
	13.52 DSCMS(28644.DSCFM)			
MOISTURE	17.92%			

STANDARD CONDITIONS- 60.F, 29.92INHG

OWENS ILLINOIS, INC.

PLANT: TOLEDO ALFALFA MILLS
 DATE: 5-26-87
 UNIT TESTED: TEST #4

	VH(IN H2O)	TS(K)	TS(F)	VS(MPS)	VS(FPS)
1	0.730	383.	230.	17.4	57.0
2	1.160	383.	230.	21.9	71.8
3	0.700	377.	220.	16.9	55.4
4	0.320	377.	220.	11.4	37.5
5	0.660	377.	220.	16.4	53.8
6	0.150	372.	210.	7.8	25.5
7	1.770	372.	210.	26.7	87.5
8	2.620	372.	210.	32.4	106.4
9	0.350	377.	220.	11.9	39.2
10	0.610	377.	220.	15.8	51.7
11	0.730	377.	220.	17.2	56.6
12	0.450	383.	230.	13.6	44.8
13	1.160	383.	230.	21.9	71.8
14	0.330	380.	225.	11.6	38.2
15	0.920	380.	225.	19.4	63.8
16	0.700	380.	225.	17.0	55.6
17	0.018	383.	230.	2.7	9.0
18	0.054	383.	230.	4.7	15.5
19	0.134	383.	230.	7.4	24.4
20	0.210	383.	230.	9.3	30.6
21	0.370	380.	225.	12.3	40.4
22	0.950	383.	230.	19.8	65.0
23	1.160	383.	230.	21.9	71.8
24	1.030	383.	230.	20.6	67.7
AVERAGE		380.	224.	15.8	51.7

PS = 747.	MMHG (29.40 INHG)	CP = 0.840
DS = 1.33 M	(52.5 IN)	VCF = 1.032
A = 1.40 SQM	(15.03 SQFT)	DH = 1.
%CO2= 2.5		MMHG (0.7 INH2O)
%CO = 0.0		PB = 747.
%O2 = 17.5		MMHG (29.40 INHG)
%N2 = 80.0		TM = 52.
		C (124.8 F)
		WC = 192.
		ML
		VMC = 1.351 CUM
		(47.690 CUFT)
		VSTD= 1.239 CUM
		(43.74 CUFT)
ST = 60.	MIN	DN = 4.78 MM
MD = 29.10		(0.188 IN)
		MS = 27.20

MG COLLECTED

PARTICULATES

386.6

OWENS ILLINOIS, INC.

PLANT: TOLEDO ALFALFA MILLS
DATE: 5-26-87
UNIT TESTED: TEST #4

	CONCENTRATION		EMISSION RATE	
	G/DSCM	GR/DSCF	G/SEC	LB/HR
PARTICULATES	0.313	0.136	4.32	34.3

FLUE GAS VOLUME 22.02 ACMS (46659.ACFM)
 13.83 DSCMS(29309.DSCFM)

MOISTURE 17.15%

STANDARD CONDITIONS- 68.F, 29.92INHG

APPENDIX 4

ISOKINETIC CALCULATIONS

SAMPLE
POINT

ΔH_p
("H₂O)

SAMPLING
TIME (min)

1	1.8	2.64
2	2.9	2.64
3	3.4	2.23
4	3.0	1.80
5	2.7	5.19
6	1.8	5.27
7	1.3	1.80
8	2.2	0.92
9	2.7	1.80
10	2.8	2.64
11	2.8	3.39
12	2.9	2.64
13	2.5	3.39
14	2.8	3.39
15	2.9	3.02
16	3.2	1.80
17	3.1	1.36
18	2.0	1.36
19	0.8	1.36
20	2.4	0.46
21	2.8	2.64
22	2.8	3.02
23	2.8	1.80
24	2.8	3.39

$\Sigma \sqrt{\Delta H_p}$: S.T. = 95.46

59.95 MIN.

1.59 = Time Weighted $\sqrt{\Delta p}$

<u>TEST NO.</u>	<u>-2-</u>	<u>-3-</u>	<u>-4-</u>
DN	<-----	0.188"	----->
BWD	<-----	17.9%	----->
Ts	<-----	224 ⁰ F	----->
Ps	<-----	29.40	----->
Ms	<-----	27.11	----->
VSTD	41.51	41.31	43.74
An(ft ²)	<-----	0.000192	----->

$$\overline{V_s} = cp \cdot 85.49 \cdot \sqrt{\Delta H_p} \cdot \sqrt{\frac{T_s}{M_s \cdot P_s}} =$$

$$0.840 \cdot 85.49 \cdot 1.59 \cdot \sqrt{\frac{684}{(27.11 \cdot 29.40)}} = 105.8 \text{ FPS}$$

$$I = \frac{T_s \cdot VSTD \cdot PSTD \cdot 100}{P_s \cdot T_{std} \cdot V_s \cdot ST \cdot An \cdot 60 \cdot (1-BWD)} = \%$$

<u>TEST NO.</u>	<u>-2-</u>	<u>-3-</u>	<u>-4-</u>
% Isokinetic Rate	91.2	90.8	96.1

APPENDIX 5

EQUIPMENT CALIBRATIONS

Date 5-28-87Meter No. 1Barometric Pressure 29.85 in Hg

D R Y G A S M E T E R			W E T		T E S T		M E T E R	
Orifice Setting	Volume	Temperatures	Volume	Temp	Pres	Time	Indicated Flow	Correction Factor

Ho <u>0.25</u>	Vm1 <u>6437.000</u>	ti1 <u>85</u>	to1 <u>80</u>	Vm <u>4.991</u> <u>196.241</u>	tw <u>78.5</u>	Pu <u>0.45</u>	t <u>10.40</u>	cfa <u>0.48</u> CF <u>1.028</u>	
	Vm2 <u>6439.000</u>	ti2 <u>91</u>	to2 <u>85</u>						tw <u>78.5</u>
	Vm <u>5.000</u>	ti <u>85.3</u>	to <u>82.5</u>						tw <u>78.5</u>
Ho <u>0.50</u>	Vm1 <u>6440.000</u>	ti1 <u>82</u>	to1 <u>86</u>	Vm <u>4.882</u> <u>196.132</u>	tw <u>78.5</u>	Pu <u>0.56</u>	t <u>7.65</u>	cfa <u>0.64</u> CF <u>1.034</u>	
	Vm2 <u>6445.000</u>	ti2 <u>100</u>	to2 <u>90</u>						tw <u>78.1</u>
	Vm <u>5.000</u>	ti <u>92</u>	to <u>88</u>						tw <u>78.3</u>
Ho <u>0.75</u>	Vm1 <u>6446.000</u>	ti1 <u>101</u>	to1 <u>91</u>	Vm <u>4.829</u> <u>196.079</u>	tw <u>78.1</u>	Pu <u>0.77</u>	t <u>6.31</u>	cfa <u>0.76</u> CF <u>1.038</u>	
	Vm2 <u>6451.000</u>	ti2 <u>110</u>	to2 <u>99</u>						tw <u>77.9</u>
	Vm <u>5.000</u>	ti <u>100.3</u>	to <u>95</u>						tw <u>78.0</u>
Ho <u>1.00</u>	Vm1 <u>6452.000</u>	ti1 <u>110</u>	to1 <u>100</u>	Vm <u>4.778</u> <u>196.028</u>	tw <u>77.9</u>	Pu <u>0.88</u>	t <u>5.52</u>	cfa <u>0.82</u> CF <u>1.043</u>	
	Vm2 <u>6457.000</u>	ti2 <u>115</u>	to2 <u>101</u>						tw <u>77.9</u>
	Vm <u>5.000</u>	ti <u>106.8</u>	to <u>100.5</u>						tw <u>77.9</u>
Ho <u>1.25</u>	Vm1 <u>6458.000</u>	ti1 <u>116</u>	to1 <u>101</u>	Vm <u>4.670</u> <u>196.170</u>	tw <u>77.9</u>	Pu <u>1.05</u>	t <u>4.9</u>	cfa <u>0.95</u> CF <u>1.046</u>	
	Vm2 <u>6463.000</u>	ti2 <u>121</u>	to2 <u>109</u>						tw <u>77.7</u>
	Vm <u>5.000</u>	ti <u>114.8</u>	to <u>105</u>						tw <u>77.8</u>

Orifice Setting	Y	K	KD
Ho	$Vm \cdot CF \cdot (Pb - Pw) \cdot (tm + 460)$	$17.65 \cdot Y \cdot Vm \cdot (Pb + Ho)$	$K \cdot \sqrt{(tm + 460) / Fd}$
	<u>13.6</u>	<u>13.6</u>	
	$Vm \cdot (Pb + Ho) \cdot (tm + 460)$	$(tm + 460) \cdot Pw / Ho$	
	<u>13.6</u>		

<u>0.25</u>	<u>1.037</u>	<u>0.964</u>	<u>4.11</u>
<u>0.50</u>	<u>1.033</u>	<u>0.912</u>	<u>3.91</u>
<u>0.75</u>	<u>1.040</u>	<u>0.897</u>	<u>3.87</u>
<u>1.00</u>	<u>1.045</u>	<u>0.882</u>	<u>3.82</u>
<u>1.25</u>	<u>1.033</u>	<u>0.861</u>	<u>3.75</u>
Average	<u>1.038</u>		<u>3.89</u>

Calibrated by

Paul Lopez

Date 5-14-87Meter No. 1Barometric Pressure 29.75 in Hg

D R Y G A S M E T E R			M E T			T E S T		M E T E R	
Orifice Settings	Volume	Temperatures	Volume	Temp	Pres	Time	Indicated Flow	Correction Factor	

Ho. <u>25</u>	Vol <u>6219.000</u> til <u>79</u> tol <u>78</u> Vn <u>26228.000</u> ti2 <u>84</u> to2 <u>80</u> Va <u>4.000</u> ta <u>80.3</u> to <u>79</u>	Vn <u>3.964</u> to <u>24.2</u> Pu <u>0.35</u> @ <u>9.55</u> <u>15 (-214)</u> <u>8.33</u>	tol <u>74.8</u> tu <u>274.6</u>	cfm <u>0.46</u>	CF <u>1.027</u>
Ho. <u>50</u>	Vol <u>6224.000</u> til <u>85</u> tol <u>81</u> Vn <u>26229.000</u> ti2 <u>92</u> to2 <u>88</u> Va <u>5.000</u> ta <u>85.8</u> to <u>83</u>	Vn <u>4.854</u> to <u>74.5</u> Pu <u>0.59</u> @ <u>7.67</u> <u>19 (-104)</u> <u>7.40</u>	tol <u>74.6</u> tu <u>274.4</u>	cfm <u>0.63</u>	CF <u>1.034</u>
Ho. <u>75</u>	Vol <u>6230.000</u> til <u>93</u> tol <u>87</u> Vn <u>26235.000</u> ti2 <u>110</u> to2 <u>91</u> Va <u>5.000</u> ta <u>92.8</u> to <u>89</u>	Vn <u>4.798</u> to <u>74.4</u> Pu <u>0.74</u> @ <u>6.35</u> <u>19 (-048)</u> <u>6.21</u>	tol <u>74.4</u> tu <u>274.4</u>	cfm <u>0.76</u>	CF <u>1.038</u>
Ho. <u>1.00</u>	Vol <u>6236.000</u> til <u>101</u> tol <u>92</u> Vn <u>26241.000</u> ti2 <u>107</u> to2 <u>98</u> Va <u>5.000</u> ta <u>99.5</u> to <u>95</u>	Vn <u>4.727</u> to <u>74.4</u> Pu <u>0.95</u> @ <u>5.50</u> <u>18 (-227)</u> <u>5.90</u>	tol <u>74.4</u> tu <u>274.4</u>	cfm <u>0.86</u>	CF <u>1.042</u>
Ho. _____	Vn1 _____ til _____ tol _____ Vn2 _____ ti2 _____ to2 _____ Va _____ ta _____ to _____	Vn _____ to _____ Pu _____ @ _____ _____	tol _____ tu _____	cfm _____	CF _____

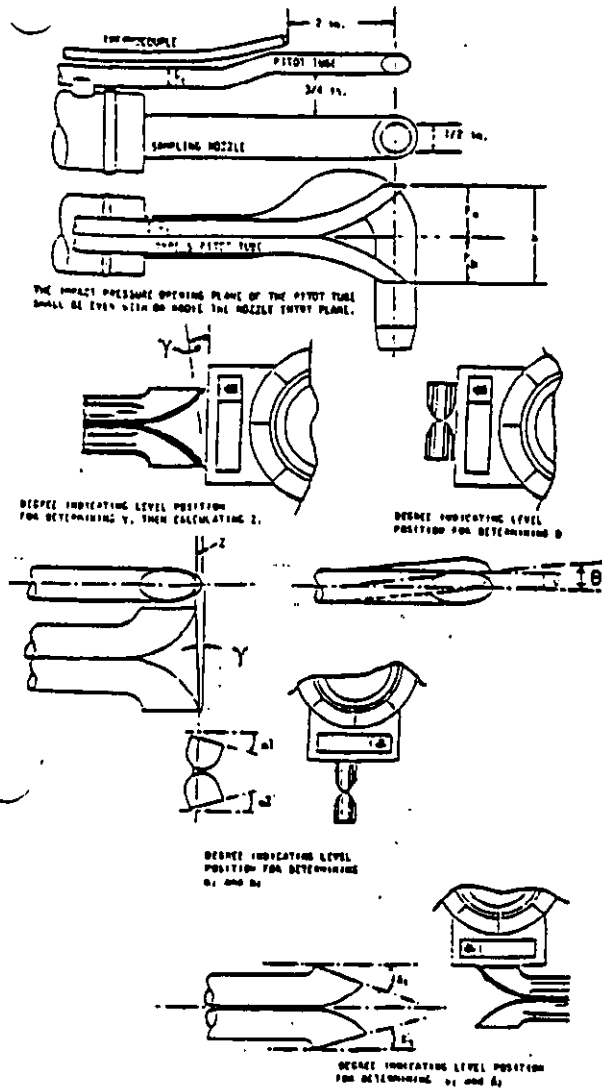
Orifice Settings	Y	X	KD
Ho	$Vn \cdot CF \cdot (Pb - Pu) \cdot (ta + 460)$ <u>13.6</u>	$17.65 \cdot Y \cdot Vn \cdot (Pb + Ho)$ <u>13.6</u>	$Ks \sqrt{(ta + 460) / Pb}$
	$Vn \cdot (Pb + Ho) \cdot (ta + 460)$ <u>13.6</u>	$(ta + 460) \cdot Ks / Ho$	
<u>0.25</u>	<u>1.027</u>	<u>.934</u>	<u>3.98</u>
<u>0.50</u>	<u>1.022</u>	<u>.908</u>	<u>3.88</u>
<u>0.75</u>	<u>1.027</u>	<u>0.888</u>	<u>3.82</u>
<u>1.00</u>	<u>1.026</u>	<u>0.878</u>	<u>3.79</u>
Average	<u>1.026</u>		<u>3.87</u>

Calibrated by Paul Sargent

PITOT TUBE INSPECTION DATA SHEET

Company Name: _____

Date 1/6/87



Yes	Level?	
No	obstructions?	
No	damaged?	
-2	$-10^\circ < \alpha_1 < +10^\circ$	
+2	$-10^\circ < \alpha_2 < +10^\circ$	
+2	$-5^\circ < \beta_1 < +5^\circ$	
-3	$-5^\circ < \beta_2 < +5^\circ$	
2	γ	
2	θ	
0.614	A	
0.307	$1.05 D_t < P_a < 1.5 D_t$	
0.307	$1.05 D_t < P_b < 1.5 D_t$	
0.257	$3/16" \leq D_t \leq 3/8"$	
0.021	$A \tan \gamma < 0.125"$	
0.021	$A \tan \theta < 0.03125"$	
Yes	$P_a = P_b \pm 0.063"$	

Comments: _____

Pitot tube/probe number 22 meets or exceeds all specifications criteria and/or applicable design features* and is hereby assigned a pitot tube calibration factor of 0.84.

Signature _____

Date 1/6/87

*See 40 CFR 60, Vol. 42, No. 160, Method 2. Verify the minimum 2 inch setback of the thermocouple and the minimum 3/4 inch separation between the pitot tube and the nozzle as shown at the top of this page.