

Note: This is a reference cited in AP 42, *Compilation of Air Pollutant Emission Factors, Volume I Stationary Point and Area Sources*. AP42 is located on the EPA web site at www.epa.gov/ttn/chief/ap42/

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AP42 Section:	9.10.1.2
Background Chapter	4
Reference:	22
Title:	Unit Nos. 1 and 2 Pulp Dryer Stacks Emission Testing Results for the February 22-26, 1993, Testing of Particulate Conducted at the American Crystal Sugar Company, Crookston, Minnesota, Bay West, Inc., St. Paul, MN, April 15, 1993.

APPENDIX U

REPORT EXCERPTS FROM REFERENCE 22

(American Crystal Sugar Company, April 15, 1993)

**Unit Nos. 1 and 2 Pulp Dryer Stacks
EMISSION TESTING RESULTS**
for the
**February 22-26, 1993 Testing of
Particulate**

conducted at the

**American Crystal Sugar Company
Crookston, Minnesota**

Submitted to:

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Submitted by:

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April 15, 1993
Project No. BW920441

1.0 EXECUTIVE SUMMARY

Bay West, Incorporated (Bay West) was contracted by American Crystal Sugar Company to perform particulate emissions compliance testing on the Unit Nos. 1 and 2 Pulp Dryer Stacks at the American Crystal Sugar Company facility located in Crookston, Minnesota. This series of testing was performed on February 22-26, 1993. The results are summarized in the following table:

TEST RESULTS SUMMARY

<u>SITE</u>	<u>PARAMETER</u>	<u>AVERAGE CONCENTRATION</u>	<u>AVERAGE MASS RATE</u>
*Test No. 1 Unit No. 1 Pulp Dryer Stack	Particulate	0.1072 gr/dscf	21.266 lb/hr 17.557
Test No. 2 Unit No. 1 Pulp Dryer Stack	Particulate	0.0710 gr/dscf	18.047 lb/hr
Test No. 3 Unit No. 2 Pulp dryer Stack	Particulate	0.0747 gr/dscf	15.091 lb/hr
Test No. 4 Unit No. 2 Pulp dryer Stack	Particulate	0.0487 gr/dscf	10.469 lb/hr 12.65
Test No. 5 Unit No. 2 Pulp dryer Stack	Particulate	0.0564 gr/dscf	12.391 lb/hr

* Run No. 3 was not conducted on test No. 1 because of Dryer System failure

TABLE 1

CLIENT: AMERICAN CRYSTAL SUGAR, CROOKSTON
SOURCE/SITE: NO. 1 PULP DRYER STACK

RESULTS OF ORSAT & MOISTURE ANALYSES - EPA METHODS 3 & 4 (%V/V)

TEST NO.: 1	RUN 1	RUN 2
DATE OF TEST	22-Feb-93	22-Feb-93
DRY BASIS (ORSAT), %		
CARBON DIOXIDE	9.03	9.67
OXYGEN	10.42	9.76
CARBON MONOXIDE	NM	NM
NITROGEN	80.55	80.57
WET BASIS (ORSAT), %		
CARBON DIOXIDE	4.67	4.95
OXYGEN	5.39	5.00
CARBON MONOXIDE	NM	NM
NITROGEN	41.65	41.26
WATER VAPOR	48.29	48.80
DRY MOLECULAR WEIGHT	29.86	29.94
WET MOLECULAR WEIGHT	24.13	24.11

NM = NOT MEASURED

TABLE 2

CLIENT: AMERICAN CRYSTAL SUGAR, CROOKSTON
 SOURCE/SITE: NO. 1 PULP DRYER STACK

RESULTS OF PARTICULATE LOADING DETERMINATIONS - EPA METHOD 5

TEST NO.: 1	RUN 1	RUN 2
DATE OF RUN	22-Feb-93	22-Feb-93
RUN START TIME	1200	1420
RUN END TIME	1340	1600
STACK STATIC PRESSURE (in. H ₂ O)	-0.60	-0.60
CROSS SECTIONAL AREA (sq. ft.)	19.634	19.634
PITOT TUBE COEFFICIENT	0.840	0.840
SAMPLE GAS MOISTURE ANALYSES		
CONDENSER (ml.)	0.00	0.00
IMPINGER (ml.)	814.00	793.00
DESSICCANT (grams)	7.00	5.00
TOTAL (grams)	821.00	798.00
SAMPLE GAS MOISTURE CONTENT (%)	48.29	48.80
DRY GAS METER COEFFICIENT	1.039	1.039
BAROMETRIC PRESSURE (in. Hg)	29.30	29.30
AVG. ORIFICE PRESSURE DROP (in. H ₂ O)	0.57	0.52
AVG. GAS METER TEMP. (degrees F)	94	94
VOLUME THROUGH GAS METER		
AT METER CONDITIONS (cf)	42.67	40.62
STANDARD CONDITIONS (dscf)	41.40	39.44
TOTAL SAMPLING TIME (min.)	96	96
NOZZLE DIAMETER (in.)	0.250	0.250
AVG. STACK GAS TEMP. (degrees F)	209	210
AVG. STACK GAS VELOCITY (ft/sec)	49.58	49.63
VOLUMETRIC FLOWRATE		
ACTUAL (acfm)	58413	58464
DRY STANDARD (dscfm)	23301	23076
ISOKINETIC VARIATION. %	106.67	102.61
PARTICULATE COLLECTED		
FILTER CATCH (g)	0.0752	0.1337
PROBE WASH (g)	0.1101	0.0984
IMPINGER CATCH (g)	0.0703	0.0722
TOTAL PARTICULATE COLLECTED (g)	0.2556	0.3043
PARTICULATE CONCENTRATION		
ACTUAL (gr/acf)	0.0380	0.0470
DRY STANDARD (gr/dscf)	0.0953	0.1191
PARTICULATE MASS RATE (lb/hr)	19.028	23.550

TABLE 3

CLIENT: AMERICAN CRYSTAL SUGAR, CROOKSTON
SOURCE/SITE: NO. 1 PULP DRYER STACK

RESULTS OF ORSAT & MOISTURE ANALYSES - EPA METHODS 3 & 4 (%V/V)

TEST NO.: 2	RUN 1	RUN 2	RUN 3
DATE OF TEST	23-Feb-93	23-Feb-93	23-Feb-93
DRY BASIS (ORSAT), %			
CARBON DIOXIDE	6.71	6.12	6.05
OXYGEN	13.15	13.86	13.93
CARBON MONOXIDE	NM	NM	NM
NITROGEN	80.14	80.02	80.02
WET BASIS (ORSAT), %			
CARBON DIOXIDE	4.08	3.76	3.75
OXYGEN	8.00	8.52	8.65
CARBON MONOXIDE	NM	NM	NM
NITROGEN	48.75	49.19	49.66
WATER VAPOR	39.17	38.53	37.93
DRY MOLECULAR WEIGHT	29.60	29.53	29.53
WET MOLECULAR WEIGHT	25.06	25.09	25.15

NM = NOT MEASURED

TABLE 4

CLIENT: AMERICAN CRYSTAL SUGAR, CROOKSTON
 SOURCE/SITE: NO. 1 PULP DRYER STACK

RESULTS OF PARTICULATE LOADING DETERMINATIONS - EPA METHOD 5

TEST NO.: 2	RUN 1	RUN 2	RUN 3
DATE OF RUN	23-Feb-93	23-Feb-93	23-Feb-93
RUN START TIME	835	1050	1315
RUN END TIME	1015	1230	1455
STACK STATIC PRESSURE (in. H ₂ O)	-0.65	-0.65	-0.65
CROSS SECTIONAL AREA (sq. ft.)	19.634	19.634	19.634
PITOT TUBE COEFFICIENT	0.840	0.840	0.840
SAMPLE GAS MOISTURE ANALYSES			
CONDENSER (ml.)	0.00	0.00	0.00
IMPINGER (ml.)	693.00	652.00	645.00
DESSICCANT (grams)	3.00	6.00	6.00
TOTAL (grams)	696.00	658.00	651.00
SAMPLE GAS MOISTURE CONTENT (%)	39.17	38.53	37.93
DRY GAS METER COEFFICIENT	1.039	1.039	1.039
BAROMETRIC PRESSURE (in. Hg)	29.40	29.40	29.40
AVG. ORIFICE PRESSURE DROP (in. H ₂ O)	0.88	0.82	0.85
AVG. GAS METER TEMP. (degrees F)	99	98	100
VOLUME THROUGH GAS METER			
AT METER CONDITIONS (cf)	52.73	51.11	51.99
STANDARD CONDITIONS (dscf)	50.91	49.44	50.17
TOTAL SAMPLING TIME (min.)	96	96	96
NOZZLE DIAMETER (in.)	0.250	0.250	0.250
AVG. STACK GAS TEMP. (degrees F)	207	208	209
AVG. STACK GAS VELOCITY (ft/sec)	52.98	52.86	52.93
VOLUMETRIC FLOWRATE			
ACTUAL (acfm)	62418	62273	62355
DRY STANDARD (dscfm)	29486	29663	29946
ISOKINETIC VARIATION. %	103.65	100.06	100.57
PARTICULATE COLLECTED			
FILTER CATCH (g)	0.0478	0.0887	0.0685
PROBE WASH (g)	0.1106	0.0961	0.1198
IMPINGER CATCH (g)	0.0604	0.0567	0.0431
TOTAL PARTICULATE COLLECTED (g)	0.2188	0.2415	0.2314
PARTICULATE CONCENTRATION			
ACTUAL (gr/acf)	0.0313	0.0359	0.0342
DRY STANDARD (gr/dscf)	0.0663	0.0754	0.0712
PARTICULATE MASS RATE (lb/hr)	16.763	19.166	18.271

TABLE 5

CLIENT: AMERICAN CRYSTAL SUGAR, CROOKSTON
SOURCE/SITE: NO. 2 PULP DRYER STACK

RESULTS OF ORSAT & MOISTURE ANALYSES - EPA METHODS 3 & 4 (%V/V)

TEST NO.: 3	RUN 1	RUN 2	RUN 3
DATE OF TEST	24-Feb-93	24-Feb-93	24-Feb-93
DRY BASIS (ORSAT), %			
CARBON DIOXIDE	5.57	5.02	4.55
OXYGEN	14.45	15.10	15.63
CARBON MONOXIDE	NM	NM	NM
NITROGEN	79.98	79.88	79.82
WET BASIS (ORSAT), %			
CARBON DIOXIDE	3.58	3.29	3.07
OXYGEN	9.30	9.88	10.53
CARBON MONOXIDE	NM	NM	NM
NITROGEN	51.47	52.29	53.77
WATER VAPOR	35.64	34.54	32.64
DRY MOLECULAR WEIGHT	29.47	29.41	29.35
WET MOLECULAR WEIGHT	25.38	25.47	25.65

NM = NOT MEASURED

TABLE 6

CLIENT: AMERICAN CRYSTAL SUGAR, CROOKSTON
 SOURCE/SITE: NO. 2 PULP DRYER STACK

RESULTS OF PARTICULATE LOADING DETERMINATIONS - EPA METHOD 5

TEST NO.: 3	RUN 1	RUN 2	RUN 3
DATE OF RUN	24-Feb-93	24-Feb-93	24-Feb-93
RUN START TIME	1010	1230	1440
RUN END TIME	1150	1410	1620
STACK STATIC PRESSURE (in. H2O)	-0.85	-0.85	-0.85
CROSS SECTIONAL AREA (sq. ft.)	12.306	12.306	12.306
PITOT TUBE COEFFICIENT	0.840	0.840	0.840
SAMPLE GAS MOISTURE ANALYSES			
CONDENSER (ml.)	0.00	0.00	0.00
IMPINGER (ml.)	428.00	683.00	637.00
DESSICCANT (grams)	2.00	9.00	7.00
TOTAL (grams)	430.00	692.00	644.00
SAMPLE GAS MOISTURE CONTENT (%)	35.64	34.54	32.64
DRY GAS METER COEFFICIENT	1.039	1.039	1.039
BAROMETRIC PRESSURE (in. Hg)	29.43	29.43	29.43
AVG. ORIFICE PRESSURE DROP (in. H2O)	0.44	1.26	1.31
AVG. GAS METER TEMP. (degrees F)	88	94	100
VOLUME THROUGH GAS METER			
AT METER CONDITIONS (cf)	37.13	63.25	64.78
STANDARD CONDITIONS (dscf)	36.57	61.77	62.61
TOTAL SAMPLING TIME (min.)	96	96	96
NOZZLE DIAMETER (in.)	0.190	0.250	0.250
AVG. STACK GAS TEMP. (degrees F)	195	195	195
AVG. STACK GAS VELOCITY (ft/sec)	61.72	61.59	61.38
VOLUMETRIC FLOWRATE			
ACTUAL (acfm)	45571	45475	45322
DRY STANDARD (dscfm)	23190	23547	24147
ISOKINETIC VARIATION. %	102.72	98.70	97.55
PARTICULATE COLLECTED			
FILTER CATCH (g)	0.0502	0.0664	0.0647
PROBE WASH (g)	0.1111	0.1714	0.1599
IMPINGER CATCH (g)	0.0296	0.0635	0.0521
TOTAL PARTICULATE COLLECTED (g)	0.1909	0.3013	0.2767
PARTICULATE CONCENTRATION			
ACTUAL (gr/acf)	0.0410	0.0390	0.0363
DRY STANDARD (gr/dscf)	0.0806	0.0753	0.0682
PARTICULATE MASS RATE (lb/hr)	16.013	15.192	14.116

TABLE 7

CLIENT: AMERICAN CRYSTAL SUGAR, CROOKSTON
SOURCE/SITE: NO. 2 PULP DRYER STACK

RESULTS OF ORSAT & MOISTURE ANALYSES - EPA METHODS 3 & 4 (%V/V)

TEST NO.: 4	RUN 1	RUN 2	RUN 3
DATE OF TEST	25-Feb-93	25-Feb-93	25-Feb-93
DRY BASIS (ORSAT), %			
CARBON DIOXIDE	3.18	3.74	3.75
OXYGEN	17.25	16.59	16.56
CARBON MONOXIDE	NM	NM	NM
NITROGEN	79.57	79.67	79.69
WET BASIS (ORSAT), %			
CARBON DIOXIDE	2.36	2.64	2.67
OXYGEN	12.79	11.72	11.79
CARBON MONOXIDE	NM	NM	NM
NITROGEN	58.98	56.29	56.73
WATER VAPOR	25.88	29.35	28.81
DRY MOLECULAR WEIGHT	29.20	29.26	29.26
WET MOLECULAR WEIGHT	26.30	25.96	26.02

NM = NOT MEASURED

TABLE 8

CLIENT: AMERICAN CRYSTAL SUGAR, CROOKSTON
 SOURCE/SITE: NO. 2 PULP DRYER STACK

RESULTS OF PARTICULATE LOADING DETERMINATIONS - EPA METHOD 5

TEST NO.: 4	RUN 1	RUN 2	RUN 3
DATE OF RUN	25-Feb-93	25-Feb-93	25-Feb-93
RUN START TIME	910	1135	1350
RUN END TIME	1150	1315	1530
STACK STATIC PRESSURE (in. H ₂ O)	-0.76	-0.76	-0.76
CROSS SECTIONAL AREA (sq. ft.)	12.306	12.306	12.306
PITOT TUBE COEFFICIENT	0.840	0.840	0.840
SAMPLE GAS MOISTURE ANALYSES			
CONDENSER (ml.)	0.00	0.00	0.00
IMPINGER (ml.)	463.00	575.00	547.00
DESSICCANT (grams)	8.00	14.00	14.00
TOTAL (grams)	471.00	589.00	561.00
SAMPLE GAS MOISTURE CONTENT (%)	25.88	29.35	28.81
DRY GAS METER COEFFICIENT	1.039	1.039	1.039
BAROMETRIC PRESSURE (in. Hg)	29.40	29.40	29.40
AVG. ORIFICE PRESSURE DROP (in. H ₂ O)	1.32	1.49	1.43
AVG. GAS METER TEMP. (degrees F)	89	100	105
VOLUME THROUGH GAS METER			
AT METER CONDITIONS (cf)	64.47	69.20	68.16
STANDARD CONDITIONS (dscf)	63.54	66.78	65.29
TOTAL SAMPLING TIME (min.)	96	96	96
NOZZLE DIAMETER (in.)	0.250	0.250	0.250
AVG. STACK GAS TEMP. (degrees F)	193	194	194
AVG. STACK GAS VELOCITY (ft/sec)	58.97	59.42	60.19
VOLUMETRIC FLOWRATE			
ACTUAL (acfm)	43538	43872	44437
DRY STANDARD (dscfm)	25591	24558	25036
ISOKINETIC VARIATION. %	93.42	102.32	98.12
PARTICULATE COLLECTED			
FILTER CATCH (g)	0.0390	0.0521	0.0430
PROBE WASH (g)	0.1360	0.1017	0.1241
IMPINGER CATCH (g)	0.0440	0.0420	0.0350
TOTAL PARTICULATE COLLECTED (g)	0.2190	0.1958	0.2021
PARTICULATE CONCENTRATION			
ACTUAL (gr/acf)	0.0313	0.0253	0.0269
DRY STANDARD (gr/dscf)	0.0532	0.0452	0.0478
PARTICULATE MASS RATE (lb/hr)	11.667	9.524	10.251

TABLE 9

CLIENT: AMERICAN CRYSTAL SUGAR, CROOKSTON
SOURCE/SITE: NO. 2 PULP DRYER STACK

RESULTS OF ORSAT & MOISTURE ANALYSES - EPA METHODS 3 & 4 (%V/V)

TEST NO.: 5	RUN 1	RUN 2	RUN 3
DATE OF TEST	26-Feb-93	26-Feb-93	26-Feb-93
DRY BASIS (ORSAT), %			
CARBON DIOXIDE	3.92	3.60	3.46
OXYGEN	16.37	16.76	16.93
CARBON MONOXIDE	NM	NM	NM
NITROGEN	79.71	79.64	79.61
WET BASIS (ORSAT), %			
CARBON DIOXIDE	2.80	2.60	2.53
OXYGEN	11.69	12.10	12.37
CARBON MONOXIDE	NM	NM	NM
NITROGEN	56.93	57.51	58.17
WATER VAPOR	28.58	27.78	26.94
DRY MOLECULAR WEIGHT	29.28	29.25	29.23
WET MOLECULAR WEIGHT	26.06	26.12	26.21

NM = NOT MEASURED

TABLE 10

CLIENT: AMERICAN CRYSTAL SUGAR, CROOKSTON
 SOURCE/SITE: NO. 2 PULP DRYER STACK

RESULTS OF PARTICULATE LOADING DETERMINATIONS - EPA METHOD 5

TEST NO.: 5	RUN 1	RUN 2	RUN 3
DATE OF RUN	26-Feb-93	26-Feb-93	26-Feb-93
RUN START TIME	805	1020	1230
RUN END TIME	945	1200	1410
STACK STATIC PRESSURE (in. H2O)	-0.82	-0.82	-0.82
CROSS SECTIONAL AREA (sq. ft.)	12.306	12.306	12.306
PITOT TUBE COEFFICIENT	0.840	0.840	0.840
SAMPLE GAS MOISTURE ANALYSES			
CONDENSER (ml.)	0.00	0.00	0.00
IMPINGER (ml.)	581.00	547.00	532.00
DESSICCANT (grams)	7.00	10.00	10.00
TOTAL (grams)	588.00	557.00	542.00
SAMPLE GAS MOISTURE CONTENT (%)	28.58	27.78	26.94
DRY GAS METER COEFFICIENT	1.039	1.039	1.039
BAROMETRIC PRESSURE (in. Hg)	29.52	29.52	29.52
AVG. ORIFICE PRESSURE DROP (in. H2O)	1.57	1.49	1.61
AVG. GAS METER TEMP. (degrees F)	93	100	104
VOLUME THROUGH GAS METER			
AT METER CONDITIONS (cf)	70.42	70.37	71.88
STANDARD CONDITIONS (dscf)	69.20	68.19	69.25
TOTAL SAMPLING TIME (min.)	96	96	96
NOZZLE DIAMETER (in.)	0.250	0.250	0.250
AVG. STACK GAS TEMP. (degrees F)	195	194	196
AVG. STACK GAS VELOCITY (ft/sec)	61.34	59.12	61.21
VOLUMETRIC FLOWRATE			
ACTUAL (acfm)	45293	43647	45191
DRY STANDARD (dscfm)	25677	25072	26167
ISOKINETIC VARIATION. %	101.40	102.33	99.57
PARTICULATE COLLECTED			
FILTER CATCH (g)	0.0480	0.0452	0.0509
PROBE WASH (g)	0.1581	0.1573	0.1656
IMPINGER CATCH (g)	0.0436	0.0412	0.0457
TOTAL PARTICULATE COLLECTED (g)	0.2497	0.2437	0.2622
PARTICULATE CONCENTRATION			
ACTUAL (gr/acf)	0.0316	0.0317	0.0338
DRY STANDARD (gr/dscf)	0.0557	0.0552	0.0584
PARTICULATE MASS RATE (lb/hr)	12.256	11.852	13.106

02/22/93

NUMBER 1 DRYER, NORTH

TIME OF DAY	1030	1130		1200	1230	1300	
SLICE RATE, TPH	198	229		239	238	231	
TOTAL PULP FLOW, TPH	56	57		59	59	64	
GRATE SPEED, %	91.58	77.70		85.41	76.27	76.69	
DRYER EXIT, °C	108.6	108.8		109.1	108.9	109.0	
ID FAN SPEED, %	85	85.0		85.0	85.0	85.0	
PULP FEED SCROLL, %	27.2	27.6	S	25.8	28.1	26.6	
PULP GATE, % CLOSED	40.0	40.0		40.0	40.0	40.0	
FD DAMPER, % OPEN	37.6	24.5	0	35.9	23.3	28.57	
RECYCLE DAMPERS, % OPEN	17.0	47.0		47.0	47.0	47.0	
RATIO SETUP	Manual	Manual	T	Manual	Manual	Manual	
DRYER THROAT	86.7	86.4		848	847	839	
DRYER EXIT, °C	105	105	#1	105	105	106	
FURNACE PRESS, IN H2O	0	-0.9		-0.6	-0.9	-0.7	
EXIT PRESS, INC H2O	1.6	1.5	(2)	-1.6	-1.6	-1.5	
DRYER AP, IN H2O	0.50	0.70		0.4	0.4	0.2	
DRUM AMPS	32	33.3	1300	35	33	35	
ID FAN, AMPS	168	168		170	169	169	
ID FLOW	61	62		61	62	61	
REC. FLOW	136	138		13.5	13.7	13.7	
M.C. AP	5.8	5.8		5.8	5.75	5.8	
BAGHOUSE AP	4.18	4.21		4.10	4.07	4.07	
ASP	8.0	8.0		8.0	8.0	7.9	
FD FLOW, AP	0.49	0.50		0.50	0.50	0.49	
#1 PULP FEED, TPH	31	31		31	31	31	01311/1314
#2 PULP FEED, TPH	24	27		29	32	31	83.48/93.33
	4.05	4.5		4.1	4.4	4.6	8572
							16" in 96 sec
	104.4	104.2		104.7	104.7	104.8	Wheel
	77.1	74.6		99.4	99.4	99.6	No 50
							3.75 4

02/22/93

NUMBER 1 DRYER, NORTH

TIME OF DAY	1330	1400		1430	1500	1530
SLICE RATE, TPH	246	229		215	151	245
TOTAL PULP FLOW, TPH	63	59		56	55	57
GRATE SPEED, %	86.25	89.14		78.12	81.66	91.48
DRYER EXIT, °C	108.5	108.4		109.1	108.6	108.7
ID FAN SPEED, %	85.0	85.0	5	85.0	85.0	85.0
PULP FEED SCROLL, %	27.8	27.6	4	27.9	31.2	31.6
PULP GATE, % CLOSED	40.0	40.0	0	40.0	40.0	40.0
FD DAMPER, % OPEN	47.08	37.66		24.92	43.96	44.14
RECYCLE DAMPERS, % OPEN	47.0	47.0	T	47.0	47.0	47.0
RATIO SETUP						
DRYER THROAT	838	818	#2	827	838	888
DRYER EXIT, °C	106	105		106	105	105
FURNACE PRESS, IN H2O	-0.1	-0.6	(a)	-0.8	-0.3	-0.1
EXIT PRESS, INC H2O	-1.5	-1.5		-1.6	-1.5	-1.6
DRYER AP, IN H2O	0.1	0	1420	0	0.1	0.2
DRUM AMPS	32	32		33.5	34	33.5
ID FAN, AMPS	170	170		168	170	168
ID FLOW	60	62		60	60	59
REC. FLOW	13.8	13.7		13.6	13.4	13.3
M.C. ΔP	5.8	5.85		5.8	5.8	5.7
BAGHOUSE ΔP	4.11	4.09		4.13	4.13	4.21
ASP	8.0	8.0		7.9	8.0	7.8
FD FLOW, AP	0.49	0.48		0.49	0.50	0.52
#1 PULP FEED, TPH	31	31		31	31	31
#2 PULP FEED, TPH	28	33		27	21	25
O ₂ , %...	4.2	4.5		4.5	4.2	3.1
BH in, °C...	105.0	104.9		105.0	105.1	105.2
out, °C...	99.4	99.6		99.7	900.6	99.7

time/wp51

Kennebec

02/23/93

NUMBER 1 DRYER (North)

TIME OF DAY	0830		0900	0930	1000	1030	
SLICE RATE, TPH	234		232	228	234	235	
TOTAL PULP FLOW, TPH	65		64	64	65	55	
GRATE SPEED, %	92.36		68.28	66.79	65.07	71.38	
DRYER EXIT, °C	107.9		108.4	107.8	107.7	108.2	
ID FAN SPEED, %	78.0		78.0	78.0	78.0	78.0	
PULP FEED SCROLL, %	20.5	S	20.1	20.2	19.8	20.5	5
PULP GATE, % CLOSED	40.0		40.0	40.0	40.0	40.0	
FD DAMPER, % OPEN	33.46	0	14.87	17.08	15.39	18.31	0
RECYCLE DAMPERS, % OPEN	47.0		47.0	47.0	47.0	47.0	
RATIO SETUP	Manual	T	Manual	Manual	Manual	Manual	T
DRYER THROAT	597		605	600	594	596	
DRYER EXIT, °C	105	#1	105	104	104	105	#2
FURNACE PRESS, IN H2O	-0.6		-0.9	-1.1	-1.0	-1.0	
EXIT PRESS, INC H2O	-1.4	(a)	-1.5	-1.6	-1.6	-1.6	(a)
DRYER ΔP, IN H2O	0.9		0.9	0.9	1.0	0.8	
DRUM AMPS	31.5	0835	30.0	30.0	31.5	31.5	1050
ID FAN, AMPS	157		158	158	159	158	
ID FLOW	61		62	60	61	63	
REC. FLOW	13.5		13.5	13.4	13.5	13.5	
M.C.ΔP	4.8		4.8	4.8	4.8	4.8	
BAGHOUSE ΔP	4.19		4.21	4.29	4.28	4.24	
ASP	8.1		8.1	8.0	8.2	8.2	
FD FLOW	0.46		0.45	0.44	0.43	0.45	
#1 PULP FEED, TPH	26		26	26	26	26	
#2 PULP FEED, TPH	27		26	27	29	25	
O ₂ , %	6.6		7.2	7.2	6.9	7.2	
BH _{in} , °C	104.5		104.3	104.4	104.5	104.5	
out, °C	78.6		78.3	99.1	99.4	99.6	

02/23/93

NUMBER 1 DRYER (North)

TIME OF DAY	1100	1130	1200	1230	1300		1330
SLICE RATE, TPH	225	224	226	223	202		231
TOTAL PULP FLOW, TPH	60	59	58	60	58		60
GRATE SPEED, %	67.78	91.95	76.69	77.47	63.41		74.50
DRYER EXIT, °C	107.7	108.3	108.2	107.8	108.2		107.5
ID FAN SPEED, %	78.0	78.0	78.0	78.0	78.0		78.0
PULP FEED SCROLL, %	20.3	20.3	20.3	20.9	20.2	S	19.8
PULP GATE, % CLOSED	40.0	40.0	40.0	40.0	40.0		40.0
FD DAMPER, % OPEN	21.15	14.22	16.90	27.58	12.86	0	27.62
RECYCLE DAMPERS, % OPEN	47.0	47.0	47.0	47.0	47.0		47.0
RATIO SETUP	—	—	—	—	—	T	—
DRYER THROAT	545	586	576	587	593		586
DRYER EXIT, °C	105	105	105	105	105	#3	105
FURNACE PRESS, IN H2O	-0.9	-1.0	-1.0	-0.7	-1.0		-0.8
EXIT PRESS, INC H2O	-1.6	-1.5	-1.5	-1.6	-1.4	②	-1.6
DRYER AP, IN H2O	0.7	0.6	0.6	0.5	0.5		0.7
DRUM AMPS	32	32	32	32	32		31
ID FAN, AMPS	158	158	158	157	158	1315	158
ID FLOW	62	60	60	60	62		60
REC. FLOW	13.6	13.5	13.5	13.3	13.5		13.5
M.C. AP	4.8	4.75	4.8	4.75	4.8		4.8
BAGHOUSE AP	4.28	4.25	4.24	4.22	4.22		4.24
ASP	8.1	7.9	8.0	8.0	8.0		7.9
FD FLOW, AP	0.44	0.44	0.45	0.45	0.43		0.45
#1 PULP FEED, TPH	26	26	26	26	26		26
#2 PULP FEED, TPH	28	31	24	26	24		25
O ₂ , %...	7.0	7.7	7.7	6.9	7.5		7.4
BH in, °C...	104.4	104.4	104.4	107.5	104.3		107.4
and, °C...	59.4	99.6	99.4	99.4	99.4		99.6

02/23/93

NUMBER 1 DRYER (North)

TIME OF DAY
SLICE RATE, TPH
TOTAL PULP FLOW, TPH
GRATE SPEED, %
DRYER EXIT, °C
ID FAN SPEED, %
PULP FEED SCROLL, %
PULP GATE, % CLOSED
FD DAMPER, % OPEN
RECYCLE DAMPERS, % OPEN
RATIO SETUP
DRYER THROAT
DRYER EXIT, °C
FURNACE PRESS, IN H2O
EXIT PRESS, INC H2O
DRYER ΔP, IN H2O
DRUM AMPS
ID FAN, AMPS
ID FLOW
REC. FLOW
M.C. ΔP
BAGHOUSE ΔP
ASP
FD FLOW, ΔP
#1 PULP FEED, TPH
#2 PULP FEED, TPH
O₂, %
BH in °C
out °C

1410
218
58
63.75
108.2
78.0
20.0
40.0
12.06
47.0
—
580
105
-1.1
-1.6
0.1
31
159
61
13.7
4.8
4.29
7.9
0.43
26
2.5
7.8
104.5
99.4

1445
211
58
76.92
107.6
78.0
20.3
40.0
29.66
47.0
—
591
104
-0.8
-1.5
0.2
31
158
59
13.6
4.75
4.26
7.9
0.44
26
26
6.9
104.4
99.4

1414-1416
62.00/92.16/80.0
8" in
57mm

WHEEL
NO 40
3.31, 3.32, 3.34
3.34

02/24/93

NUMBER 2 DRYER (South)

TIME OF DAY	0830	0910	0935	1000		1030	1106
SLICE RATE, TPH	227	221	228	225		225	234
TOTAL PULP FLOW, TPH	68	55	63	62		63	66
GRATE SPEED, %	70.07	79.50	79.16	73.56 77.77		71.66	74.40
DRYER EXIT, °C	100.3	100.5	100.1	99.9		99.9	99.8
ID FAN SPEED, %	70.0	70.0	70.0	70.0		70.0	70.0
PULP FEED SCROLL, %	103.3	103.3	103.3	103.3		103.3	103.3
PULP GATE, % CLOSED	68.25	-3.34	-3.34	60.00	5	61.51	61.35
FD DAMPER, % OPEN	16.20	24.79	28.96	27.73		19.95	27.66
RECYCLE DAMPERS, % OPEN	26.0	65.0	49.0	45.0	0	45.0	45.0
RATIO SETUP	Manual	Manual	Manual	Manual		Manual	Manual
DRYER THROAT	704	608	612	651	T	653	649
DRYER EXIT, °C	101	101	100	100		100	100
FURNACE PRESS, IN H2O	-1.3	-1.2	-1.2	-1.2	#1	-1.3	-1.2
EXIT PRESS, INC H2O	-1.0	-1.0	-1.1	-1.0		-1.1	-1.1
DRYER ΔP, IN H2O	1.2	1.2	1.1	1.1	(2)	1.2	1.2
DRUM AMPS	28	27.5	26.5	27		27.5	27
ID FAN, AMPS	154	154	154	154	1010	154	154
ID FLOW	32	34	33	32		33	32.5
REC. FLOW	5.0	10.6	9.6	8.7		8.6	8.3
M.C. ΔP	4.05	4.05	4.05	4.05		4.05	3.8
BAGHOUSE ΔP	4.78	4.70	4.69	4.69		4.65	4.67
ASP	7.4	6.9	7.25	7.4		6.7	7.3
FD FLOW, ΔP	1.03	1.03	1.03	1.03		1.03	1.03
#1 PULP FEED, TPH	32	28	33	31		31	32
#2 PULP FEED, TPH	26	27	30	27		27	30
	9.5	8.8	8.8	8.8		9.0	8.3
O ₂ , %							
BH in °C	103.0	102.5	102.4	102.6		102.8	102.5
out °C	93.7	93.9	93.5	93.3		93.3	93.5

02/24/93

NUMBER 2 DRYER (South)

TIME OF DAY	1400	1430	1500	1530	1600	1630
SLICE RATE, TPH	228	229	230	229	220	217
TOTAL PULP FLOW, TPH	59	58	57	56	55	57
GRATE SPEED, %	75.13	79.22	78.28	67.50	62.26	74.86
DRYER EXIT, °C	100.0	99.8	100.0	100.0	99.8	99.8
ID FAN SPEED, %	70.0	70.0	70.0	70.0	70.0	70.0
PULP FEED SCROLL, %	103.3	103.3	103.3	103.3	103.3	103.3
PULP GATE, % CLOSED	60.0	60.0	60.0	60.0	60.0	60.0
FD DAMPER, % OPEN	22.66	28.96	26.35	22.11	12.58	20.42
RECYCLE DAMPERS, % OPEN	45.0	45.0	45.0	45.0	45.0	45.0
RATIO SETUP	Manual	Manual	Manual	Manual	Manual	Manual
DRYER THROAT	58.2	57.7	57.3	52.3	50.4	55.9
DRYER EXIT, °C	100	100	100	100	100	101
FURNACE PRESS, IN H2O	-1.2	-1.2	-1.3	-1.4	-1.4	-1.3
EXIT PRESS, INC H2O	-1.1	-1.1	-1.1	-1.1	-1.1	-1.1
DRYER AP, IN H2O	1.3	1.3	1.3	1.2	1.2	1.3
DRUM AMPS	26.5	27	27	27	27	27
ID FAN, AMPS	155	156	154	154	154	154
ID FLOW	33	33	32.5	34	34	33.5
REC. FLOW	9.3	9.4	9.6	8.7	9.0	9.6
M.C.A.P	2.9	3.1	2.9	3.95	3.95	3.95
BAGHOUSE AP	4.62	4.62	4.54	4.54	4.62	4.50
ASP	6.9	7.1	7.2	7.0	7.1	7.2
FD FLOW, AP	1.03	1.03	1.03	1.03	1.03	1.03
#1 PULP FEED, TPH	30	30	30	30	29	31
#2 PULP FEED, TPH	27	27	27	26	27	27
O ₂ , %...	9.8	9.4	9.5	10.2	10.4	9.4
BH _{in} , °C...	103.2	103.2	103.2	103.2	103.2	103.4
out, °C...	93.5	93.7	93.4	93.4	93.4	94.0

02/25/93

NUMBER 2 DRYER (South)

TIME OF DAY	0900		0930	1000		1030	1100
SLICE RATE, TPH	233		233	227		160	234
TOTAL PULP FLOW, TPH	61		52	54		55	58
GRATE SPEED, %	67.10		62.42	64.50		67.18	77.83
DRYER EXIT, °C	98.9		98.9	98.8		98.8	98.8
ID FAN SPEED, %	70.0		70.0	70.0		70.0	70.0
PULP FEED SCROLL, %	103.3		103.3	103.3		103.3	103.3
PULP GATE, % CLOSED	65.00	5	60.00	60.00		60.00	60.00
FD DAMPER, % OPEN	17.16		13.23	15.03		17.60	25.96
RECYCLE DAMPERS, % OPEN	45.0	0	45.0	45.0		45.0	45.0
RATIO SETUP	Manual		Manual	Manual		Manual	Manual
DRYER THROAT	473	Ta	405	356		384	433
DRYER EXIT, °C	99		99	99		99	99
FURNACE PRESS, IN H2O	-1.3	#1	-1.4	-1.4		-1.4	-1.3
EXIT PRESS, INC H2O	-1.0		-0.8	-0.9		-0.9	-1.1
DRYER AP, IN H2O	1.1	Q	1.3	1.3		1.3	1.3
DRUM AMPS	26.5		26.0	26.5		26.5	27
ID FAN, AMPS	156	0910	156	155		154	154
ID FLOW	34		35	35		35	34
REC. FLOW	10		9.3	9.4		9.5	9.5
M.C. AP	4.05		4.05	4.05		4.05	4.05
BAGHOUSE AP	4.76		4.72	4.78		4.74	4.67
ASP	7.0		7.2	6.9		7.0	7.0
FD FLOW, AP	1.03		1.03	1.03		1.03	1.03
#1 PULP FEED, TPH	35		33	33		34	33
#2 PULP FEED, TPH	22		19	22		23	26
O ₂ , %	10.9		12.6	12.4		11.7	11.0
BHim, °C	102.8		102.8	102.7		102.8	103.0
and, °C	91.6		91.3	91.6		91.8	92.4
						1040-1044	
						68.54/67.69	
						68.34	
						8" in 99 sec	

02/25/93

NUMBER 2 DRYER (South)

TIME OF DAY	1130		1200	1230	1300	1315	1330
SLICE RATE, TPH	230		226	230	228	228	220
TOTAL PULP FLOW, TPH	60		64	67	66	64	63
GRATE SPEED, %	68.28		79.73	74.92	64.08	73.41	67.89
DRYER EXIT, °C	98.9		98.7	98.9	99.0	98.8	98.8
ID FAN SPEED, %	70.0		70.0	70.0	70.0	70.0	70.0
PULP FEED SCROLL, %	103.3		103.3	103.3	103.3	103.3	103.3
PULP GATE, % CLOSED	62.03		70.75	69.97	70.65	70.65	69.50
FD DAMPER, % OPEN	21.43	5	32.68	24.74	13.02	21.38	19.09
RECYCLE DAMPERS, % OPEN	45.0		45.0	45.0	45.0	45.0	45.0
RATIO SETUP	Manual	0	Manual	Manual	Manual	Manual	Manual
DRYER THROAT	467		482	439	427	429	434
DRYER EXIT, °C	99	T	99	99	99	99	99
FURNACE PRESS, IN H2O	-1.4		-1.2	-1.4	-1.5	-1.4	-1.4
EXIT PRESS, INC H2O	-0.9	#2	-1.2	-1.1	-1.1	-1.2	-1.0
DRYER AP, IN H2O	1.3		1.1	1.3	1.3	1.2	1.2
DRUM AMPS	27	(2)	27	27		27.5	26.5
ID FAN, AMPS	154		154	154		155	154
ID FLOW	35	1135	34	33		33.5	33
REC. FLOW	9.4		9.4	9.6		9.4	9.3
M.C. AP	4.05		4.05	4.05		4.05	4.05
BAGHOUSE AP	4.66		4.61	4.63		4.57	4.63
ASP	7.0		7.0	7.2		7.0	6.9
FD FLOW, AP	1.03		1.03	1.03	1.03	1.03	1.03
#1 PULP FEED, TPH	35		35	35	36	36	36
#2 PULP FEED, TPH	26		22	22	22	21	20
O ₂ , %	10.4		10.7	11.5		11.3	11.4
BH _{in} , %	103.2		103.1	103.2		103.4	103.5
out, %	92.6		92.6	92.6		92.7	92.8
				1230-1234			
				68.17/69.58			
				68.15			

8-in in 94 sec.

02/25/93

NUMBER 2 DRYER (South)

TIME OF DAY	1400	1430	1500	1530	
SLICE RATE, TPH	228	230	226	225	
TOTAL PULP FLOW, TPH	61	61	60	58	
GRATE SPEED, %	78.33	61.30	65.05	65.67	
DRYER EXIT, °C	99.1	98.9	98.9	98.8	
ID FAN SPEED, %	70.0	70.0	70.0	70.0	
PULP FEED SCROLL, %	103.3	103.3	103.3	103.3	
PULP GATE, % CLOSED	67.0	69.76	69.76	69.76	
FD DAMPER, % OPEN	30.29	14.04	13.78	16.54	
RECYCLE DAMPERS, % OPEN	45.0	45.0	45.0	45.0	
RATIO SETUP	Manual	Manual	Manual	Manual	
DRYER THROAT	440	455	445	404	
DRYER EXIT, °C	100	99	99	99	
FURNACE PRESS, IN H2O	-1.3	-1.5	-1.5	-1.5	
EXIT PRESS, INC H2O	-1.1	-1.1	-1.0	-1.0	
DRYER AP, IN H2O	1.2	1.3	1.3	1.2	
DRUM AMPS	27	26	27	26.5	
ID FAN, AMPS	154	154	154	154	
ID FLOW	35	33.5	34.5	36	
REC. FLOW	9.5	9.4	9.3	9.2	
M.C. ΔP	4.05	4.05	4.05	4.05	
BAGHOUSE ΔP	4.57	4.53	4.54	4.57	
ASP	7.1	7.0	6.9	6.8	
FD FLOW, ΔP	1.03	1.03	1.03	1.03	
#1 PULP FEED, TPH	35	35	35	35	
#2 PULP FEED, TPH	24	22	21	21	
O ₂ , %...	10.7	11.0	11.2	11.7	
BH in, °C...	103.5	103.2	103.3	103.3	
out, °C...	93.2	93.1	93.0	92.6	
	1404		Manual		
	46.53/49.46		Pressure =		
	54.83		0.14/0.16		

8" in 25 sec.
- in H2O above gate

02226/93

NUMBER 2 DRYER (South)

TIME OF DAY	1330	1400	1430	1500				
SLICE RATE, TPH	200	204	218	215				
TOTAL PULP FLOW, TPH	56	51	57	57				
GRATE SPEED, %	71.19	72.03	92.89	80.72				
DRYER EXIT, °C	99.8	99.9	100.0	99.9				
ID FAN SPEED, %	72.0	72.0	72.0	72.0				
PULP FEED SCROLL, %	103.3	103.3	103.3	103.3				
PULP GATE, % CLOSED	60.0	60.0	60.0	60.0				
FD DAMPER, % OPEN	20.96	19.11	42.76	28.59				
RECYCLE DAMPERS, % OPEN	45.0	45.0	45.0	45.0				
RATIO SETUP	Manual	Manual	Manual	Manual				
DRYER THROAT	285	427	485	478				
DRYER EXIT, °C	100	100	100	100				
FURNACE PRESS, IN H2O	-1.3	-1.3	-1.0	-1.2				
EXIT PRESS, INC H2O	-1.1	-1.1	-1.3	-1.3				
DRYER AP, IN H2O	1.3	1.2	1.2	1.2				
DRUM AMPS	26.5	26.5	27	26.5				
ID FAN, AMPS	156	156	155	156				
ID FLOW	34.5	34.5	33	33.5				
REC. FLOW	9.6	9.5	9.5	9.6				
M.C. AP	4.05	4.05	4.05	4.05				
BAGHOUSE AP	4.71	4.66	4.60	4.61				
ASP	6.8	6.9	6.8	7.0				
FD FLOW, AP	1.03	1.03	1.03	1.03				
#1 PULP FEED, TPH	29	30	33	34				
#2 PULP FEED, TPH	24	24	27	24				
O ₂ , %	11.9	11.2	10.0	11.0				
BH in, °C	102.8	103.2	103.2	103.6				
out, °C	93.5	93.8	94.2	93.9				
Exhaust	48.0							
Exhaust	48.0							

Filename: BEET22.WQ1

Date: 19-Jan-95

Facility: American Crystal Sugar

Location: Crookston, Minnesota

Source: No. 1 pulp dryer (coal-fired) w/multiclones and stack filter system

Test date: February 22, 1993

D. Emission Data/Mass Flux Rates/Emission Factors

Test ID	Parameter	Units	Values reported				
			Run 1	Run 2	Run 3	Run 4	Run 5
1	Stack temperature	Deg F	209	210	207	208	209
No. 1 pulp dryer	Pressure	in. HG	29.30	29.30	29.40	29.40	29.40
	Moisture	%	48.29	48.80	39.17	38.53	37.93
	Oxygen	%	10.42	9.765	13.15	13.86	13.93
	Volumetric flow, actual	acfm	58413	58464	62418	62273	62355
	Volumetric flow, standard*	dscfm	23345	23101	29534	29731	30016
	Isokinetic variation	%	106.67	102.61	103.65	100.06	100.57
Pulp dryer feed rate		TPH	31.0	31.0	26.0	26.0	26.0
NEED TO CHECK W/PLANT!!							
Pollutant concentrations:							
	Total PM	G/dscf	0.0953	0.1191	0.0663	0.0754	0.0712
	Filterable PM	G/dscf	0.0656	0.0908	0.0480	0.0577	0.0579
	Condensable organic PM	G/dscf	0.0297	0.0283	0.0183	0.0177	0.0133
	CO2	% vol	9.03	9.67	6.71	6.12	6.05
Pollutant mass flux rates:							
	Filterable PM	lb/hr	13.1	18.0	12.2	14.7	14.9
	Condensable organic PM	lb/hr	5.94	5.60	4.63	4.51	3.41
	CO2	lb/hr	14447	15309	13581	12470	12445
Emission factors (ENGLISH UNITS):							
	Filterable PM	lb/ton	0.42	0.58	0.47	0.57	0.57
	Condensable organic PM	lb/ton	0.19	0.18	0.18	0.17	0.13
	CO2	lb/ton	466	494	522	480	479
Emission factors (METRIC UNITS):							
	Filterable PM	kg/Mg	0.21	0.29	0.23	0.28	0.29
	Condensable organic PM	kg/Mg	0.096	0.090	0.089	0.087	0.066
	CO2	kg/Mg	233	247	261	240	239
							AVERAGE
							0.52
							0.17
							488
							AVERAGE
							0.26
							0.086
							244

*DSCFM BASED ON A STANDARD TEMPERATURE OF 68 DEGREES FAHRENHEIT

Filename: BEET22A.WQ1

Date: 19-Jan-95

Facility: American Crystal Sugar

Location: Crookston, Minnesota

Source: No. 2 pulp dryer (coal-fired) w/multiclones and stack filter system

Test date: February 24-25, 1993

D. Emission Data/Mass Flux Rates/Emission Factors

Test ID	Parameter	Units	Values reported								
			Run 1	Run 2	Run 3	Run 4	Run 5	Run 6	Run 7	Run 8	Run 9
No. 2 pulp dryer	Stack temperature	Deg F	195	195	195	193	194	194	195	194	196
	Pressure	in. HG	29.43	29.43	29.43	29.40	29.40	29.40	29.52	29.52	29.52
	Moisture	%	35.64	34.54	32.64	25.88	29.35	28.81	28.58	27.78	26.94
	Oxygen	%	14.45	15.1	15.63	17.25	16.59	16.56	16.37	16.76	16.93
	Volumetric flow, actual	acfm	45571	45475	45322	43538	43872	44437	45293	43647	45191
Pulp dryer feed rate NEED TO CHECK W/PLANT!!	Volumetric flow, standard*	dscfm	23256	23603	24207	25640	24589	25096	25728	25109	26219
	Isokinetic variation	%	102.72	98.7	97.55	93.42	102.32	98.12	101.4	102.33	99.57
	TPH	TPH	28.0	27.0	26.8	23.2	22.0	22.0	24.3	24.0	23.5
Pollutant concentrations:											
	Total PM	G/dscf	0.0806	0.0753	0.0682	0.0532	0.0452	0.0478	0.0557	0.0552	0.0584
	Filterable PM	G/dscf	0.0681	0.0594	0.0554	0.0425	0.0355	0.0395	0.0460	0.0459	0.0482
	Condensable organic PM	G/dscf	0.0125	0.0159	0.0128	0.0107	0.0097	0.008278	0.009726	0.009332	0.0102
	CO2	% vol	5.57	5.02	4.55	3.18	3.74	3.75	3.92	3.6	3.46
Pollutant mass flux rates:											
	Filterable PM	lb/hr	13.6	12.0	11.5	9.3	7.5	8.5	10.1	9.9	10.8
	Condensable organic PM	lb/hr	2.49	3.21	2.66	2.35	2.04	1.78	2.14	2.01	2.29
	CO2	lb/hr	8877	8120	7548	5588	6303	6450	6912	6195	6217
Emission factors (ENGLISH UNITS):											
	Filterable PM	lb/ton	0.48	0.45	0.43	0.40	0.34	0.39	0.42	0.41	0.46
	Condensable organic PM	lb/ton	0.089	0.12	0.10	0.10	0.093	0.081	0.088	0.084	0.097
	CO2	lb/ton	317	301	282	241	286	293	285	258	265
Emission factors (METRIC UNITS):											
	Filterable PM	kg/Mg	0.24	0.22	0.21	0.20	0.17	0.19	0.21	0.21	0.23
	Condensable organic PM	kg/Mg	0.044	0.059	0.050	0.051	0.046	0.040	0.044	0.042	0.049
	CO2	kg/Mg	159	150	141	120	143	147	143	129	132
											AVERAGE
											0.42
											0.095
											281
											AVERAGE
											0.21
											0.047
											140

*DSCFM BASED ON A STANDARD TEMPERATURE OF 68 DEGREES FAHRENHEIT

LAB NO: 3425
SOURCE: 2 Dryer stack
SITE: Crookston
LOCATION: ACS

TEST NO: 5
RUN NO: 3
DATE: 3-9-93
ANALYST: R. Hesser
Reviewed: 3-12-93 SWP

FILTERS

<u>Lab No.</u>	<u>Final Wt. (g)</u>	<u>Tare Wt. (g)</u>	<u>Gain (g)</u>
<u>33999</u>	<u>0.6313</u>	<u>- 0.5804</u>	<u>= 0.0509</u>
			TOTAL <u>0.0509</u>

Probe & Front Half Wash

<u>Lab No.</u>	<u>Final Wt. (g)</u>	<u>Tare Wt. (g)</u>	<u>Gain (g)</u>
<u>33998</u>	<u>21.2981</u>	<u>- 21.1313</u>	<u>= 0.1668</u>
BLANK <u>0.158</u> (1) * <u>0.0079</u> (g/l) = <u>- 0.0012</u> (g)			
			CORRECTED TOTAL <u>0.1656</u>

IMPINGER CATCH

<u>Lab No.</u>	<u>Final Wt. (g)</u>	<u>Tare Wt. (g)</u>	<u>Gain (g)</u>
<u>34000</u>	<u>135.4257</u>	<u>- 135.3790</u>	<u>= 0.0467</u>
BLANK <u>0.730</u> (1) * <u>0.0013</u> (g/l) = <u>- 0.0010</u>			
			CORRECTED TOTAL <u>0.0457</u>

SUMMARY OF CORRECTED TOTALS (g)

<u>RUN NO.</u>	<u>FILTER</u>	<u>PROBE WASH</u>	<u>IMP. CATCH</u>	<u>TOTAL</u>
<u>3</u>	<u>0.0509</u>	<u>+ 0.1656</u>	<u>+ 0.0457</u>	<u>= 0.2622</u>

LAB NO: 3425
 SOURCE: 2 Dryer stack
 SITE: Crookston
 LOCATION: ACS

 TEST NO: 5
 RUN NO: 2
 DATE: 3-9-93
 ANALYST: R. Hesser
 Reviewed: 3-12-93 SWP
FILTERS

<u>Lab No.</u>	<u>Final Wt.(g)</u>	<u>Tare Wt.(g)</u>	<u>Gain (g)</u>
<u>33946</u>	<u>0.6250</u>	<u>0.5798</u>	<u>0.0452</u>
TOTAL			<u>0.0452</u>

Probe & Front Half Wash

<u>Lab No.</u>	<u>Final Wt.(g)</u>	<u>Tare Wt.(g)</u>	<u>Gain (g)</u>
<u>33995</u>	<u>21.1627</u>	<u>21.0042</u>	<u>0.1585</u>
BLANK <u>0.158</u> (1) * <u>0.0079</u> (g/l) = <u>0.0012</u> (g)			
CORRECTED TOTAL			<u>0.1573</u>

IMPINGER CATCH

<u>Lab No.</u>	<u>Final Wt.(g)</u>	<u>Tare Wt.(g)</u>	<u>Gain (g)</u>
<u>33997</u>	<u>140.7792</u>	<u>140.7370</u>	<u>0.0422</u>
BLANK <u>0.740</u> (1) * <u>0.0013</u> (g/l) = <u>0.0010</u>			
CORRECTED TOTAL			<u>0.0412</u>

SUMMARY OF CORRECTED TOTALS (g)

<u>RUN NO.</u>	<u>FILTER</u>	<u>PROBE WASH</u>	<u>IMP. CATCH</u>	<u>TOTAL</u>
<u>2</u>	<u>0.0452</u>	<u>0.1573</u>	<u>0.0412</u>	<u>0.2437</u>

LAB NO: 3425
SOURCE: 2 Paper stock
SITE: Crookston
LOCATION: ACS

TEST NO: 5
RUN NO: 1
DATE: 3-9-93
ANALYST: R. Hesse
Reviewed: 3-12-93 SWP

FILTERS

<u>Lab No.</u>	<u>Final Wt.(g)</u>	<u>Tare Wt.(g)</u>	<u>Gain (g)</u>
<u>33993</u>	<u>0.6248</u>	<u>0.5768</u>	<u>0.0480</u>
TOTAL <u>0.0480</u>			

Probe & Front Half Wash

<u>Lab No.</u>	<u>Final Wt.(g)</u>	<u>Tare Wt.(g)</u>	<u>Gain (g)</u>
<u>33992</u>	<u>21.2666</u>	<u>21.1075</u>	<u>0.1591</u>
BLANK <u>0.130</u> (l) * <u>0.0079</u> (g/l) = <u>0.0010</u> (g)			
CORRECTED TOTAL <u>0.1581</u>			

IMPINGER CATCH

<u>Lab No.</u>	<u>Final Wt.(g)</u>	<u>Tare Wt.(g)</u>	<u>Gain (g)</u>
<u>33994</u>	<u>134.8221</u>	<u>134.7775</u>	<u>0.0446</u>
BLANK <u>0.800</u> (l) * <u>0.0013</u> (g/l) = <u>0.0010</u>			
CORRECTED TOTAL <u>0.0436</u>			

SUMMARY OF CORRECTED TOTALS (g)

<u>RUN NO.</u>	<u>FILTER</u>	<u>PROBE WASH</u>	<u>IMP. CATCH</u>	<u>TOTAL</u>
<u>1</u>	<u>0.0480</u>	<u>+ 0.1581</u>	<u>+ 0.0436</u>	<u>= 0.2497</u>

LAB NO: 3425
SOURCE: 2 Dryer stack
SITE: Crookston
LOCATION: ACS

TEST NO: 4
RUN NO: 3
DATE: 3-9-93
ANALYST: R. Hessler
Reviewed: 3-12-93 swp

FILTERS

Lab No.	Final Wt. (g)	Tare Wt. (g)	Gain (g)
<u>33990</u>	<u>0.6197</u>	<u>0.5767</u>	<u>0.0430</u>
TOTAL			<u>0.0430</u>

Probe & Front Half Wash

Lab No.	Final Wt. (g)	Tare Wt. (g)	Gain (g)
<u>33989</u>	<u>21.3167</u>	<u>21.1917</u>	<u>0.1250</u>
BLANK <u>0.116</u> (1) * <u>0.0079</u> (g/l) =			<u>0.0009</u> (g)
CORRECTED TOTAL			<u>0.1241</u>

IMPINGER CATCH

Lab No.	Final Wt. (g)	Tare Wt. (g)	Gain (g)
<u>33991</u>	<u>142.8937</u>	<u>142.8577</u>	<u>0.0360</u>
BLANK <u>0.750</u> (1) * <u>0.0013</u> (g/l) =			<u>0.0010</u>
CORRECTED TOTAL			<u>0.0350</u>

SUMMARY OF CORRECTED TOTALS (g)

RUN NO.	FILTER	PROBE WASH	IMP. CATCH	TOTAL
<u>3</u>	<u>0.0430</u>	<u>0.1241</u>	<u>0.0350</u>	<u>0.2021</u>

LAB NO: 3425
SOURCE: 2 Dryer stack
SITE: Cookston
LOCATION: ACS

TEST NO: 4
RUN NO: 2
DATE: 3-9-93
ANALYST: R. Hessler
Reviewed: 3-12-93 SWP

FILTERS

<u>Lab No.</u>	<u>Final Wt. (g)</u>	<u>Tare Wt. (g)</u>	<u>Gain (g)</u>
<u>33987</u>	<u>0.6317</u>	<u>0.5796</u>	<u>0.0521</u>
			TOTAL <u>0.0521</u>

Probe & Front Half Wash

<u>Lab No.</u>	<u>Final Wt. (g)</u>	<u>Tare Wt. (g)</u>	<u>Gain (g)</u>
<u>33986</u>	<u>21.1446</u>	<u>21.0421</u>	<u>0.1025</u>
BLANK <u>0.106</u> (1) * <u>0.0079</u> (g/l) = <u>0.0008</u> (g)			
			CORRECTED TOTAL <u>0.1017</u>

IMPINGER CATCH

<u>Lab No.</u>	<u>Final Wt. (g)</u>	<u>Tare Wt. (g)</u>	<u>Gain (g)</u>
<u>33988</u>	<u>136.5129</u>	<u>136.4699</u>	<u>0.0430</u>
BLANK <u>0.770</u> (1) * <u>0.0013</u> (g/l) = <u>0.0010</u>			
			CORRECTED TOTAL <u>0.0420</u>

SUMMARY OF CORRECTED TOTALS (g)

<u>RUN NO.</u>	<u>FILTER</u>	<u>PROBE WASH</u>	<u>IMP. CATCH</u>	<u>TOTAL</u>
<u>2</u>	<u>0.0521</u>	<u>0.1017</u>	<u>0.0420</u>	<u>0.1958</u>

LAB NO: 3425
 SOURCE: 2 Dryer Stack
 SITE: Crookston
 LOCATION: ACS

 TEST NO: 4
 RUN NO: 1
 DATE: 2-9-93
 ANALYST: K. Hessler
 Reviewed: 3-12-93 SWP
FILTERS

<u>Lab No.</u>	<u>Final Wt. (g)</u>	<u>Tare Wt. (g)</u>	<u>Gain (g)</u>
<u>33984</u>	<u>0.6164</u>	<u>0.5774</u>	<u>0.0390</u>
TOTAL			<u>0.0390</u>

Probe & Front Half Wash

<u>Lab No.</u>	<u>Final Wt. (g)</u>	<u>Tare Wt. (g)</u>	<u>Gain (g)</u>
<u>33983</u>	<u>21.5310</u>	<u>21.3938</u>	<u>0.1372</u>
BLANK <u>0.156</u> (l) * <u>0.0079</u> (g/l) = <u>0.0012</u> (g)			
CORRECTED TOTAL			<u>0.1360</u>

IMPINGER CATCH

<u>Lab No.</u>	<u>Final Wt. (g)</u>	<u>Tare Wt. (g)</u>	<u>Gain (g)</u>
<u>33985</u>	<u>137.8034</u>	<u>137.7586</u>	<u>0.0448</u>
BLANK <u>0.660</u> (l) * <u>0.0013</u> (g/l) = <u>0.0008</u>			
CORRECTED TOTAL			<u>0.0440</u>

SUMMARY OF CORRECTED TOTALS (g)

<u>RUN NO.</u>	<u>FILTER</u>	<u>PROBE WASH</u>	<u>IMP. CATCH</u>	<u>TOTAL</u>
<u>1</u>	<u>0.0390</u>	<u>0.1360</u>	<u>0.0440</u>	<u>0.2190</u>

LAB NO: 3425
SOURCE: #2 Dryer stack
SITE: Crookston
LOCATION: ACS

TEST NO: 3
RUN NO: 3
DATE: 3-9-93
ANALYST: R. Hessler
Reviewed: 3-12-93 SWP

FILTERS

Lab No.	Final Wt. (g)	Tare Wt. (g)	Gain (g)
<u>33981</u>	<u>0.6449</u>	<u>0.5802</u>	<u>0.0647</u>
			TOTAL <u>0.0647</u>

Probe & Front Half Wash

Lab No.	Final Wt. (g)	Tare Wt. (g)	Gain (g)
<u>33980</u>	<u>21.6041</u>	<u>21.4429</u>	<u>0.1612</u>
BLANK <u>0.164</u> (1) * <u>0.0079</u> (g/l) = <u>0.0013</u> (g)			
			CORRECTED TOTAL <u>0.1599</u>

IMPINGER CATCH

Lab No.	Final Wt. (g)	Tare Wt. (g)	Gain (g)
<u>33982</u>	<u>139.8264</u>	<u>139.7732</u>	<u>0.0532</u>
BLANK <u>0.830</u> (1) * <u>0.0013</u> (g/l) = <u>0.0011</u>			
			CORRECTED TOTAL <u>0.0521</u>

SUMMARY OF CORRECTED TOTALS (g)

RUN NO.	FILTER	PROBE WASH	IMP. CATCH	TOTAL
<u>3</u>	<u>0.0647</u>	<u>0.1599</u>	<u>0.0521</u>	<u>0.2767</u>

LAB NO: 3425
SOURCE: #2 Dryer Stack
SITE: Crookston
LOCATION: ACS

TEST NO: 3
RUN NO: 2
DATE: 3-9-93
ANALYST: R. Hesser
Reviewed: 3-12-93 SWP

FILTERS

Lab No.	Final Wt. (g)	Tare Wt. (g)	Gain (g)
<u>33978</u>	<u>0.6466</u>	<u>0.5802</u>	<u>0.0664</u>
TOTAL			<u>0.0664</u>

Probe & Front Half Wash

Lab No.	Final Wt. (g)	Tare Wt. (g)	Gain (g)
<u>33977</u>	<u>21.6810</u>	<u>21.5082</u>	<u>0.1728</u>
BLANK <u>0.184</u> (1) * <u>0.0079</u> (g/l) = <u>0.0014</u> (g)			
CORRECTED TOTAL			<u>0.1714</u>

IMPINGER CATCH

Lab No.	Final Wt. (g)	Tare Wt. (g)	Gain (g)
<u>33979</u>	<u>140.6425</u>	<u>140.5779</u>	<u>0.0646</u>
BLANK <u>0.870</u> (1) * <u>0.0013</u> (g/l) = <u>0.0011</u>			
CORRECTED TOTAL			<u>0.0635</u>

SUMMARY OF CORRECTED TOTALS (g)

RUN NO.	FILTER	PROBE WASH	IMP. CATCH	TOTAL
<u>2</u>	<u>0.0664</u>	<u>0.1714</u>	<u>0.0635</u>	<u>0.3013</u>

LAB NO: 3425
SOURCE: #2 Dryer Stack
SITE: Crookston
LOCATION: ACS

TEST NO: 3
RUN NO: 1
DATE: 3-9-93
ANALYST: R. Hesser
Reviewed: 3-12-93 SWP

FILTERS

<u>Lab No.</u>	<u>Final Wt. (g)</u>	<u>Tare Wt. (g)</u>	<u>Gain (g)</u>
<u>33975</u>	<u>0.6330</u>	<u>- 0.5828</u>	<u>= 0.0502</u>
			TOTAL <u>0.0502</u>

Probe & Front Half Wash

<u>Lab No.</u>	<u>Final Wt. (g)</u>	<u>Tare Wt. (g)</u>	<u>Gain (g)</u>
<u>33974</u>	<u>21.1795</u>	<u>- 21.0674</u>	<u>= 0.1121</u>
BLANK <u>0.126</u> (l) * <u>0.0079</u> (g/l) = <u>0.0010</u> (g)			
			CORRECTED TOTAL <u>0.1111</u>

IMPINGER CATCH

<u>Lab No.</u>	<u>Final Wt. (g)</u>	<u>Tare Wt. (g)</u>	<u>Gain (g)</u>
<u>33976</u>	<u>136.6337</u>	<u>- 136.6033</u>	<u>= 0.0304</u>
BLANK <u>0.640</u> (l) * <u>0.0013</u> (g/l) = <u>0.0008</u>			
			CORRECTED TOTAL <u>0.0296</u>

SUMMARY OF CORRECTED TOTALS (g)

<u>RUN NO.</u>	<u>FILTER</u>	<u>PROBE WASH</u>	<u>IMP. CATCH</u>	<u>TOTAL</u>
<u>1</u>	<u>0.0502</u>	<u>+ 0.1111</u>	<u>+ 0.0296</u>	<u>= 0.1909</u>

LAB NO: 3425
SOURCE: 1 Dryer stack
SITE: Crookston
LOCATION: ACS

TEST NO: 2
RUN NO: 3
DATE: 3-9-93
ANALYST: R. Hessler
Reviewed: 3-12-93 SWP

FILTERS

<u>Lab No.</u>	<u>Final Wt.(g)</u>	<u>Tare Wt.(g)</u>	<u>Gain (g)</u>
<u>33972</u>	<u>0.6501</u>	<u>- 0.5816</u>	<u>= 0.0685</u>
			TOTAL <u>0.0685</u>

Probe & Front Half Wash

<u>Lab No.</u>	<u>Final Wt.(g)</u>	<u>Tare Wt.(g)</u>	<u>Gain (g)</u>
<u>33971</u>	<u>21.6865</u>	<u>- 21.5654</u>	<u>= 0.1211</u>
BLANK <u>0.164</u> (1) * <u>0.0071</u> (g/l) = <u>- 0.0013</u> (g)			
			CORRECTED TOTAL <u>0.1198</u>

IMPINGER CATCH

<u>Lab No.</u>	<u>Final Wt.(g)</u>	<u>Tare Wt.(g)</u>	<u>Gain (g)</u>
<u>33973</u>	<u>140.1096</u>	<u>- 140.0654</u>	<u>= 0.0442</u>
BLANK <u>0.840</u> (1) * <u>0.0013</u> (g/l) = <u>- 0.0011</u>			
			CORRECTED TOTAL <u>0.0431</u>

SUMMARY OF CORRECTED TOTALS (g)

<u>RUN NO.</u>	<u>FILTER</u>	<u>PROBE WASH</u>	<u>IMP. CATCH</u>	<u>TOTAL</u>
<u>3</u>	<u>0.0685</u>	<u>+ 0.1198</u>	<u>+ 0.0431</u>	<u>= 0.2314</u>

LAB NO: 3425
SOURCE: 1 Dryer stack
SITE: Crookston
LOCATION: ACS

TEST NO: 2
RUN NO: 2
DATE: 3-9-93
ANALYST: R. Hessler
Reviewed: 3-12-93 SWP

FILTERS

<u>Lab No.</u>	<u>Final Wt.(g)</u>	<u>Tare Wt.(g)</u>	<u>Gain (g)</u>
<u>33469</u>	<u>0.6673</u>	<u>- 0.5786</u>	<u>= 0.0887</u>
			TOTAL <u>0.0887</u>

Probe & Front Half Wash

<u>Lab No.</u>	<u>Final Wt.(g)</u>	<u>Tare Wt.(g)</u>	<u>Gain (g)</u>
<u>33968</u>	<u>21.6283</u>	<u>- 21.5309</u>	<u>= 0.0974</u>
BLANK <u>0.168</u> (1) * <u>0.0079</u> (g/l) = <u>- 0.0013</u> (g)			
			CORRECTED TOTAL <u>0.0961</u>

IMPINGER CATCH

<u>Lab No.</u>	<u>Final Wt.(g)</u>	<u>Tare Wt.(g)</u>	<u>Gain (g)</u>
<u>33970</u>	<u>138.5096</u>	<u>- 138.4518</u>	<u>= 0.0578</u>
BLANK <u>0.850</u> (1) * <u>0.0013</u> (g/l) = <u>- 0.0011</u>			
			CORRECTED TOTAL <u>0.0567</u>

SUMMARY OF CORRECTED TOTALS (g)

<u>RUN NO.</u>	<u>FILTER</u>	<u>PROBE WASH</u>	<u>IMP. CATCH</u>	<u>TOTAL</u>
<u>2</u>	<u>0.0887</u>	<u>+ 0.0961</u>	<u>+ 0.0567</u>	<u>= 0.2415</u>

LAB NO: 3425
SOURCE: 1 Pulp Drier Stack
SITE: Crookston
LOCATION: ACS

TEST NO: 2
RUN NO: 1
DATE: 3-9-93
ANALYST: R. Hessler
Reviewed: 3-12-93 SWP

FILTERS

Lab No.	Final Wt. (g)	Tare Wt. (g)	Gain (g)
<u>33966</u>	<u>0.6240</u>	<u>0.5762</u>	<u>0.0478</u>
TOTAL			<u>0.0478</u>

Probe & Front Half Wash

Lab No.	Final Wt. (g)	Tare Wt. (g)	Gain (g)
<u>33965</u>	<u>21.6543</u>	<u>21.5425</u>	<u>0.1118</u>
BLANK <u>0.154</u> (l) * <u>0.0079</u> (g/l) =			<u>0.0012</u> (g)
CORRECTED TOTAL			<u>0.1106</u>

IMPINGER CATCH

Lab No.	Final Wt. (g)	Tare Wt. (g)	Gain (g)
<u>33967</u>	<u>141.6480</u>	<u>141.5864</u>	<u>0.0616</u>
BLANK <u>0.910</u> (l) * <u>0.0013</u> (g/l) =			<u>0.0012</u>
CORRECTED TOTAL			<u>0.0604</u>

SUMMARY OF CORRECTED TOTALS (g)

RUN NO.	FILTER	PROBE WASH	IMP. CATCH	TOTAL
<u>1</u>	<u>0.0478</u>	<u>0.1106</u>	<u>0.0604</u>	<u>0.2188</u>

LAB NO: 3425
SOURCE: 1 Pulp Dryer Stack
SITE: Crookston
LOCATION: ACS

TEST NO: 1
RUN NO: 2
DATE: 3-9-93
ANALYST: R. Hessler
Reviewed: 3-12-93 swp

FILTERS

<u>Lab No.</u>	<u>Final Wt. (g)</u>	<u>Tare Wt. (g)</u>	<u>Gain (g)</u>
<u>33962</u>	<u>0.7806</u>	<u>- 0.6469</u>	<u>= 0.1337</u>
			TOTAL <u>0.1337</u>

Probe & Front Half Wash

<u>Lab No.</u>	<u>Final Wt. (g)</u>	<u>Tare Wt. (g)</u>	<u>Gain (g)</u>
<u>33961</u>	<u>20.7114</u>	<u>- 20.6118</u>	<u>= 0.0996</u>
BLANK <u>0.154</u> (1) * <u>0.0079</u> (g/l) = <u>- 0.0012</u> (g)			
			CORRECTED TOTAL <u>0.0984</u>

IMPINGER CATCH

<u>Lab No.</u>	<u>Final Wt. (g)</u>	<u>Tare Wt. (g)</u>	<u>Gain (g)</u>
<u>33963</u>	<u>136.8678</u>	<u>- 136.7943</u>	<u>= 0.0735</u>
BLANK <u>1.010</u> (1) * <u>0.0013</u> (g/l) = <u>- 0.0013</u>			
			CORRECTED TOTAL <u>0.0722</u>

SUMMARY OF CORRECTED TOTALS (g)

<u>RUN NO.</u>	<u>FILTER</u>	<u>PROBE WASH</u>	<u>IMP. CATCH</u>	<u>TOTAL</u>
<u>62</u>	<u>0.1337</u>	<u>+ 0.0984</u>	<u>+ 0.0722</u>	<u>= 0.3043</u>

LAB NO: 3425
SOURCE: 1 Alp Dryer stack
SITE: Crookston
LOCATION: ACS

TEST NO: 1
RUN NO: 1
DATE: 3-9-93
ANALYST: R. Hessler
Reviewed: 3-12-93 SWP

FILTERS

<u>Lab No.</u>	<u>Final Wt.(g)</u>	<u>Tare Wt.(g)</u>	<u>Gain (g)</u>
<u>33958</u>	<u>0.6985</u>	<u>- 0.6233</u>	<u>= 0.0752</u>
			TOTAL <u>0.0752</u>

Probe & Front Half Wash

<u>Lab No.</u>	<u>Final Wt.(g)</u>	<u>Tare Wt.(g)</u>	<u>Gain (g)</u>
<u>33957</u>	<u>21.5134</u>	<u>- 21.4022</u>	<u>= 0.1112</u>
BLANK <u>0.144</u> (1) * <u>0.0079</u> (g/l) = <u>- 0.0011</u> (g)			
			CORRECTED TOTAL <u>0.1101</u>

IMPINGER CATCH

<u>Lab No.</u>	<u>Final Wt.(g)</u>	<u>Tare Wt.(g)</u>	<u>Gain (g)</u>
<u>33959</u>	<u>135.7372</u>	<u>- 135.6656</u>	<u>= 0.0716</u>
BLANK <u>1.020</u> (1) * <u>0.0013</u> (g/l) = <u>- 0.0013</u>			
			CORRECTED TOTAL <u>0.0703</u>

SUMMARY OF CORRECTED TOTALS (g)

<u>RUN NO.</u>	<u>FILTER</u>	<u>PROBE WASH</u>	<u>IMP. CATCH</u>	<u>TOTAL</u>
<u>1</u>	<u>0.0752</u>	<u>+ 0.1101</u>	<u>+ 0.0703</u>	<u>= 0.2556</u>

2.0 INTRODUCTION

Bay West personnel conducted particulate emission compliance testing on the Unit Nos. 1 and 2 Pulp Dryer Stacks at the American Crystal Sugar Company located in Crookston, Minnesota. On-site testing was performed on February 22-26, 1993 by a two-member Bay West team consisting of Dwayne Smith and Dan Phipps. Coordination between the facility operations and testing activities was provided by Dave Noble of the Crookston facility through direct contact with the test team leader. The testing consisted of multiple independent 96-minute determinations for particulate with concurrent integrated gas sampling for Orsat analyses at each site.

The objectives of this project were to quantify particulate emissions and compare them to applicable air emissions regulations stipulated by state and federal guidelines. Special provisions for this testing included, but were not limited to, operating the facility at or near maximum capacity.

Results are reported in the next section followed by an explanation of the test procedures used and a description of the process under investigation. All supporting information is included in the appendices.

3.0 RESULTS

Results of particulate determinations and gas composition are found in Tables 1 through 10. The results of additional air flow profiles taken at the Dryer Aspiration Ducts and the Recycle Ducts are found in Appendix 6.

Test No. 1, Run No. 3, was cancelled due to dryer disturbances but no problems were encountered in the sampling or analyses of emission samples on the other tests. After complete review of the test results, we believe that the values reported herein are an accurate representation of the actual source conditions during the time of testing.

The wet catch was analyzed for condensible organic particulate via a chloroform/diethyl ether extraction. Three 25-ml portions of diethyl ether were used in the extraction which were then evaporated at room temperature and desiccated to a constant weight. Gravimetric results were then added to the dry catch results (filter and probe wash explained above) to calculate the final particulate concentrations.

5.0 PROCESS DESCRIPTION

Pulp Dryers Nos. 1 and 2 at the American Crystal Sugar facility in Crookston, Minnesota are of rotary drum design and are used to dry sugar-beet pulp. The drums are heated by coal-fired furnaces. Pollution control is facilitated by multiclones and stack filter systems. A portion of the exhaust gas from the multiclones may be recycled to the rotary drums to maintain proper operating temperatures. Schematics are included in Figures 1 and 2.