



AIR POLLUTION TESTING, INC.

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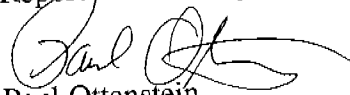
Filler Rooms Diagnostic VOC Test Report for Coors Brewing Company

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Introduction

Air Pollution Testing was contracted by Coors Brewing Company to conduct a series of source emissions tests on the air inlets and outlets from the #3 Bottle Filler, #5 Can Filler, #6 Can Filler, and #9 Can Filler rooms. The purpose of the testing was to determine mass flow rates of volatile organic compounds (VOCs), believed to be primarily ethanol, at each location. The testing was conducted intermittently from 12-2-92 through 12-16-92.

Summary of Procedures

VOC testing was conducted in accordance with "EPA Method 25A - Measurement of Total Gaseous Organic Concentration Using a Flame Ionization Analyzer" as detailed in Code of Federal Regulations, Title 40, Part 60, Appendix A. At each location (except #9 Can Filler), three one hour sampling runs were conducted using a JUM Model 3-100 Flame Ionization Analyzer (FIA). A sample of duct gas was continuously extracted through a heated PTFE sample line and pumped directly into the inlet port of the analyzer. The concentration of VOCs (expressed as parts per million by volume on a wet basis as propane) was displayed on the front panel of the analyzer and recorded on a strip chart. At the beginning of each sampling day, the analyzer was calibrated with hydrocarbon-free air and a high level calibration gas, and challenged with a mid level calibration gas to verify the linearity of response. After each one hour sampling period, the analyzer was again challenged with the hydrocarbon-free air and one of the calibration gases to quantify zero and span drift for the previous sampling period. At this point the analyzer was also recalibrated as necessary. The strip chart data from each sampling period was averaged in one to three minute increments, and reported as parts per million by volume on a wet basis as propane, with all data corrected for zero and span drift. Identical sampling and analysis procedures were conducted at the #9 Can Filler location, with longer sampling times and less frequent calibration cycles. To ensure accurate data collection, all calibration gases were prepared and certified in accordance with EPA Protocol 1, and were introduced to the analyzer at the sampling probe tip. Additionally, during each sampling period, Tedlar gas bags were filled with duct gas from each inlet location and analyzed immediately using the FIA. Tedlar gas bag samples were also occasionally collected and analyzed from points around the filler rooms.

Concurrent with each method 25A sampling run, methods 1, 2, and 4 were used to determine the duct gas velocity and volumetric flow rates at the inlet and outlet locations. Each filler room tested had a single outlet duct where room air was pulled out of the room, and two or three inlet ducts where air was pumped into the room. At all locations, temperature and differential pressure traverses were conducted in accordance with method 2 along a grid of sampling points selected in accordance with method 1. Method 4 sampling runs were conducted at all outlet locations to determine the outlet duct gas moisture content. Inlet locations were assumed to have negligible moisture content, and ambient concentrations of carbon dioxide (0.0%) and oxygen (20.9%) were assumed for all locations. This data was combined to determine the gas velocity and volumetric flow rate at each location.

Additional Notes

Propane to Ethanol Conversion

Although flame ionization analyzers (FIAs) are designed to detect carbon atoms in organic molecules without respect to the remainder of the molecule, experiments have demonstrated that FIA response is somewhat dependent on molecular structure. Because the VOC emissions from the filler rooms are believed to be primarily ethanol, the data presented in the results section has been corrected from propane calibrated FIA data to theoretical ethanol values. This can be achieved through consideration of stoichiometry and published carbon-basis response factors, or an empirical conversion factor can be experimentally determined. In this report, the conversion factor was determined experimentally using the same FIA used for all field measurements. Experimental determination of the response factor was conducted using syringe injections of precisely known masses of reagent grade ethanol into Tedlar gas bags. The gas bags were filled with a known volume of ambient air using an SKC personal sampling pump with a NIST traceable bubble calibrator. The mass of ethanol injected was determined by tare and final weights of the syringe using a certified 0.1 mg analytical balance. The volume of air was determined using the average of six flow measurements recorded at the beginning and end of each filling, along with the total filling time. The liquid/gas samples were allowed to evaporate and mix, and were then pumped into the analyzer, which was calibrated with EPA Protocol 1 propane calibration gases immediately before and after bag sampling. A total of 5 bag samples were prepared and analyzed. An average conversion factor was calculated and used to convert other propane calibrated analyzer data to ethanol values. The experimental conversion factor was compared with correction values published by the manufacturer. These values agreed to within 5.3%.

Theoretical Mass Emission Rates

Because the filler rooms are necessarily maintained at positive pressure with respect to the brewery facilities surrounding them, the total air flows measured at the inlet ducts to each filler room were greater than the flows measured at the outlet locations, with the difference presumably leaking out of the rooms at any non-sealed points. Consequently, the total VOC emissions from the rooms were calculated using the concentrations measured at the outlets, and the flows measured at the inlets. These calculations assume that the air within the rooms was well mixed, and no significant VOC concentration gradients existed in the rooms. To demonstrate the validity of this assumption, several Tedlar gas bag samples were collected at points around the rooms during the sampling programs. The results indicated that the VOC concentration of the escaping air was typically similar to the outlet measurements. The "Theoretical Total" values calculate the emissions using the outlet VOC concentrations and the inlet flows. The "Theoretical from Filling" values calculate the emissions using the outlet minus inlet concentrations and the inlet flows.

#9 Can Filler Inlet Flow

During the first 2 days of VOC testing at the #9 Can Filler location, the #2 inlet duct did not have adequately sized sampling ports along the vertical axis for temperature and differential pressure measurements. Only a single port at the center of the underside of the duct was adequate. This port was sampled at three points selected in accordance with method 1, and the data recorded for subsequent conversion. At a later date, three adequate ports along the vertical axis had been installed. Method 2 sampling traverses were conducted at these ports as well as at the previously sampled port on the underside of the duct, with a total of three traverses conducted from each port. The ratio of the average square root of the differential pressure of the three ports along the vertical axis to the average square root of the differential pressure of the three points along the underside port was calculated. The average ratio from the three runs was used to convert the center-line method 2 data collected in the first set of sampling runs to true method 2 data for the entire duct. The method 2 traverses of the entire duct indicated that using only the center-line data would substantially overstate the total duct flow.

#5 Can Filler Inlet Flow

At the #5 Can Filler inlet locations, ports for method 2 sampling were not installed at the time of the testing. During subsequent testing at another location, method 2 data was collected from the #5 Can inlet ducts and used for calculations.

Results

The results of the testing are presented in the following tables. Any testing parameters not presented in the tables may be found in Appendix 1 - Sample Calculations and Testing Parameters.

Coors Brewing Company #3 Bottle Filler 12-2-92 VOC Mass Emission Rates				
<u>Field Data</u>	Run #1	Run #2	Run #3	Averages
<u>Outlet</u>				
VOC conc. (ppm wet)	28.6	30.3	30.6	29.8
% H ₂ O	1.3	0.9	0.5	0.9
volumetric flow rate (dscfm)	1499	1494	1528	1507
<u>Inlet #1</u>				
VOC conc. (ppm)	2.0	3.5	3.0	2.8
volumetric flow rate (dscfm)	1874	2359	1923	2052
<u>Inlet #2</u>				
VOC conc. (ppm)	2.5	1.0	1.5	1.7
volumetric flow rate (dscfm)	1871	1825	1879	1858
<u>Inlet #3</u>				
VOC conc. (ppm)	3.0	3.0	3.0	3.0
volumetric flow rate (dscfm)	1829	2333	2646	2269
<u>Production</u>				
beer filling (bbl/hr)	85.3	85.3	85.3	85.3
<u>Calculations</u>	Run #1	Run #2	Run #3	Averages
<u>Theoretical Total</u>				
VOC lb/hr as propane	1.11	1.37	1.36	1.28
VOC lb/hr as ethanol	2.78	3.43	3.41	3.21
VOC lb/bbl as ethanol	0.0326	0.0402	0.0400	0.0376
<u>Theoretical from Filling</u>				
VOC lb/hr as propane	1.01	1.25	1.25	1.17
VOC lb/hr as ethanol	2.54	3.13	3.13	2.93
VOC lb/bbl as ethanol	0.0298	0.0367	0.0367	0.0344

Table 1 - VOC Mass Emission Rates
#3 Bottle Filler

Results (continued)

Coors Brewing Company #5 Can Filler 12-2-92 VOC Mass Emission Rates				
<u>Field Data</u>	Run #1	Run #2	Run #3	Averages
<u>Outlet</u>				
VOC conc. (ppm wet)	93.4	87.2	85.5	88.7
% H ₂ O	1.3	0.9	0.5	0.9
volumetric flow rate (dscfm)	3130	3116	3009	3085
<u>Inlet #1</u>				
VOC conc. (ppm)	1.0	1.0	1.3	1.1
volumetric flow rate (dscfm)*	2108	2129	2090	2109
<u>Inlet #2</u>				
VOC conc. (ppm)**	1.0	1.0	1.3	1.1
volumetric flow rate (dscfm)*	2615	3059	2526	2733
<u>Production</u>				
beer filling (bbl/hr)	207.7	207.7	207.7	207.7
<u>Calculations</u>	Run #1	Run #2	Run #3	Averages
<u>Theoretical Total</u>				
VOC lb/hr as propane	3.07	3.13	2.72	2.98
VOC lb/hr as ethanol	7.69	7.86	6.82	7.46
VOC lb/bbl as ethanol	0.0370	0.0378	0.0329	0.0359
<u>Theoretical from Filling</u>				
VOC lb/hr as propane	3.04	3.10	2.68	2.94
VOC lb/hr as ethanol	7.61	7.77	6.72	7.37
VOC lb/bbl as ethanol	0.0366	0.0374	0.0324	0.0355
* - measured 1-27-93				
** - not measured due to bag leak, inlet #1 data assumed				

Table 2 - VOC Mass Emission Rates
#5 Can Filler

Two Tedlar bag samples collected under the filler room doors during run #3 measured 65.0 and 67.0 ppm as propane.

Results (continued)

Coors Brewing Company
#6 Can Filler
12-16-92
VOC Mass Emission Rates

Field Data		Run #1	Run #2	Run #3	Averages
<u>Outlet</u>	VOC conc. (ppm wet)	113.5	111.1	111.5	112.0
	% H2O	1.5	0.8	1.1	1.2
	volumetric flow rate (dscfm)	1927	1930	1847	1901
<u>Inlet #1</u>	VOC conc. (ppm)	1.5	1.5	2.5	1.8
	volumetric flow rate (dscfm)	3766	1660	1030	2152
<u>Inlet #2</u>	VOC conc. (ppm)*	1.0	1.0	1.0	1.0
	volumetric flow rate (dscfm)	1803	1643	2335	1927
<u>Production</u>	beer filling (bbl/hr)	216.7	216.7	216.7	216.7
Calculations		Run #1	Run #2	Run #3	Averages
<u>Theoretical Total</u>					
	VOC lb/hr as propane	4.41	2.54	2.61	3.18
	VOC lb/hr as ethanol	11.04	6.37	6.53	7.98
	VOC lb/bbl as ethanol	0.0510	0.0294	0.0301	0.0368
<u>Theoretical from Filling</u>					
	VOC lb/hr as propane	4.35	2.51	2.57	3.15
	VOC lb/hr as ethanol	10.91	6.29	6.44	7.88
	VOC lb/bbl as ethanol	0.0504	0.0290	0.0297	0.0364

* - run #1 not measured due to bag leak, average of runs 2 and 3 assumed

Table 3 - VOC Mass Emission Rates
#6 Can Filler

Three Tedlar gas bag samples collected under the filler room door during runs #1, #2, and #3 measured 144.0 ppm, 128.0 ppm, and 142.0 ppm as propane respectively.

Results (continued)

The #9 Can Filler was sampled continuously from 07:30 on 12-2-92 through 00:12 on 12-5-92. The results of the testing are presented as two hour averages in the following tables. Flow data are the averages of 5 sampling traverses. Production data is an average for the entire period.

Coors Brewing Company #9 Can Filler 12-3-92 through 12-5-92 VOC Mass Emission Rates						
<u>Field Data</u>	hrs 1-2	hrs 3-4	hrs 5-6	hrs 7-8	hrs 9-10	Averages
<u>Outlet</u>						
VOC conc. (ppm wet)	7.6	8.6	12.0	14.8	39.6	16.5
% H ₂ O	0.6	0.6	0.6	0.6	0.6	0.6
volumetric flow rate (dscfm)	2359	2359	2359	2359	2359	2359
<u>Inlet #1</u>						
VOC conc. (ppm)	2.5	2.5	2.5	2.5	2.5	2.5
volumetric flow rate (dscfm)	6392	6392	6392	6392	6392	6392
<u>Inlet #2</u>						
VOC conc. (ppm)	2.7	2.7	2.7	2.7	2.7	2.7
volumetric flow rate (dscfm)	2379	2379	2379	2379	2379	2379
<u>Production</u>						
beer filling (bbl/hr)	*	*	*	*	153.8	153.8
<u>Calculations</u>	hrs 1-2	hrs 3-4	hrs 5-6	hrs 7-8	hrs 9-10	Averages
<u>Theoretical Total</u>						
VOC lb/hr as propane	0.46	0.52	0.73	0.90	2.40	1.00
VOC lb/hr as ethanol	1.15	1.31	1.82	2.25	6.01	2.51
VOC lb/bbl as ethanol	*	*	*	*	0.0391	0.0391
<u>Theoretical from Filling</u>						
VOC lb/hr as propane	0.31	0.37	0.57	0.74	2.24	0.85
VOC lb/hr as ethanol	0.77	0.92	1.43	1.86	5.62	2.12
VOC lb/bbl as ethanol	*	*	*	*	0.0366	0.0366
* - filler room sterilization was conducted for the first eight hours of sampling, no beer filling took place during this time						

Table 4 - VOC Mass Emission Rates
 #9 Can Filler
 (hours 1 through 10)

Results (continued)

Coors Brewing Company #9 Can Filler 12-3-92 through 12-5-92 VOC Mass Emission Rates						
Field Data	hrs 11-12	hrs 13-14	hrs 15-16	hrs 17-18	hrs 19-20	Averages
Outlet						
VOC conc. (ppm wet)	43.0	42.9	33.4	49.1	46.3	42.9
% H ₂ O	0.6	0.6	0.6	0.6	0.6	0.6
volumetric flow rate (dscfm)	2359	2359	2359	2359	2359	2359
Inlet #1						
VOC conc. (ppm)	2.5	2.5	2.5	2.5	2.5	2.5
volumetric flow rate (dscfm)	6392	6392	6392	6392	6392	6392
Inlet #2						
VOC conc. (ppm)	2.7	2.7	2.7	2.7	2.7	2.7
volumetric flow rate (dscfm)	2379	2379	2379	2379	2379	2379
Production						
beer filling (bbl/hr)	153.8	153.8	153.8	153.8	153.8	153.8
Calculations	hrs 11-12	hrs 13-14	hrs 15-16	hrs 17-18	hrs 19-20	Averages
Theoretical Total						
VOC lb/hr as propane	2.60	2.60	2.02	2.97	2.80	2.60
VOC lb/hr as ethanol	6.53	6.51	5.07	7.45	7.03	6.52
VOC lb/bbl as ethanol	0.0424	0.0423	0.0330	0.0484	0.0457	0.0424
Theoretical from Filling						
VOC lb/hr as propane	2.45	2.44	1.87	2.82	2.65	2.45
VOC lb/hr as ethanol	6.14	6.12	4.68	7.06	6.64	6.13
VOC lb/bbl as ethanol	0.0399	0.0398	0.0304	0.0459	0.0432	0.0399

Table 5 - VOC Mass Emission Rates
 #9 Can Filler
 (hours 11 through 20)

Results (continued)

Coors Brewing Company
#9 Can Filler
12-3-92 through 12-5-92
VOC Mass Emission Rates

<u>Field Data</u>		hrs 21-22	hrs 23-24	hrs 25-26	hrs 27-28	hrs 29-30	Averages
<u>Outlet</u>							
	VOC conc. (ppm wet)	48.4	39.5	35.7	36.3	41.2	40.2
	% H ₂ O	0.6	0.6	0.6	0.6	0.6	0.6
	volumetric flow rate (dscfm)	2359	2359	2359	2359	2359	2359
<u>Inlet #1</u>							
	VOC conc. (ppm)	2.5	2.5	2.5	2.5	2.5	2.5
	volumetric flow rate (dscfm)	6392	6392	6392	6392	6392	6392
<u>Inlet #2</u>							
	VOC conc. (ppm)	2.7	2.7	2.7	2.7	2.7	2.7
	volumetric flow rate (dscfm)	2379	2379	2379	2379	2379	2379
<u>Production</u>							
	beer filling (bbl/hr)	153.8	153.8	153.8	153.8	153.8	153.8
<u>Calculations</u>							
<u>Theoretical Total</u>							
	VOC lb/hr as propane	2.93	2.39	2.16	2.20	2.50	2.44
	VOC lb/hr as ethanol	7.35	6.00	5.42	5.51	6.25	6.10
	VOC lb/bbl as ethanol	0.0478	0.0390	0.0352	0.0358	0.0407	0.0397
<u>Theoretical from Filling</u>							
	VOC lb/hr as propane	2.78	2.24	2.01	2.04	2.34	2.28
	VOC lb/hr as ethanol	6.96	5.61	5.03	5.12	5.87	5.72
	VOC lb/bbl as ethanol	0.0452	0.0365	0.0327	0.0333	0.0381	0.0372

Table 6 - VOC Mass Emission Rates
#9 Can Filler
(hours 21 through 30)

Two Tedlar gas bag samples collected under the filler room door during hour 27 measured 58.5 ppm and 69.0 ppm as propane.

Results (continued)

Coors Brewing Company #9 Can Filler 12-3-92 through 12-5-92 VOC Mass Emission Rates						
Field Data	hrs 31-32	hrs 33-34	hrs 35-36	hrs 37-38	hrs 39-40	Averages
Outlet						
VOC conc. (ppm wet)	37.9	50.6	35.9	45.2	49.7	43.9
% H2O	0.6	0.6	0.6	0.6	0.6	0.6
volumetric flow rate (dscfm)	2359	2359	2359	2359	2359	2359
Inlet #1						
VOC conc. (ppm)	2.5	2.5	2.5	2.5	2.5	2.5
volumetric flow rate (dscfm)	6392	6392	6392	6392	6392	6392
Inlet #2						
VOC conc. (ppm)	2.7	2.7	2.7	2.7	2.7	2.7
volumetric flow rate (dscfm)	2379	2379	2379	2379	2379	2379
Production						
beer filling (bbl/hr)	153.8	153.8	153.8	153.8	153.8	153.8
Calculations	hrs 31-32	hrs 33-34	hrs 35-36	hrs 37-38	hrs 39-40	Averages
Theoretical Total						
VOC lb/hr as propane	2.30	3.06	2.17	2.74	3.01	2.66
VOC lb/hr as ethanol	5.75	7.68	5.45	6.86	7.54	6.66
VOC lb/bbl as ethanol	0.0374	0.0499	0.0354	0.0446	0.0490	0.0433
Theoretical from Filling						
VOC lb/hr as propane	2.14	2.91	2.02	2.58	2.86	2.50
VOC lb/hr as ethanol	5.36	7.29	5.06	6.47	7.16	6.27
VOC lb/bbl as ethanol	0.0349	0.0474	0.0329	0.0421	0.0465	0.0408

Table 7 - VOC Mass Emission Rates
#9 Can Filler
(hours 31 through 40)

Two Tedlar gas bag samples collected under the filler room door during hour 33 measured 87.0 ppm and 83.0 ppm as propane.

Results (continued)

The 33 hour averages exclude the data collected during the first eight hours of sampling, when no beer filling was conducted.

Coors Brewing Company #9 Can Filler 12-3-92 through 12-5-92 VOC Mass Emission Rates		
<u>Field Data</u>	hour 41	33 hour Averages (exclude sterilization)
<u>Outlet</u>		
VOC conc. (ppm wet)	39.8	42.1
% H ₂ O	0.6	0.6
volumetric flow rate (dscfm)	2359	2359
<u>Inlet #1</u>		
VOC conc. (ppm)	2.5	2.5
volumetric flow rate (dscfm)	6392	6392
<u>Inlet #2</u>		
VOC conc. (ppm)	2.7	2.7
volumetric flow rate (dscfm)	2379	2379
<u>Production</u>		
beer filling (bbl/hr)	153.8	153.8
<u>Calculations</u>	hour 41	33 hour Averages (exclude sterilization)
<u>Theoretical Total</u>		
VOC lb/hr as propane	2.41	2.55
VOC lb/hr as ethanol	6.04	6.39
VOC lb/bbl as ethanol	0.0393	0.0416
<u>Theoretical from Filling</u>		
VOC lb/hr as propane	2.26	2.40
VOC lb/hr as ethanol	5.65	6.00
VOC lb/bbl as ethanol	0.0368	0.0390

Table 8 - VOC Mass Emission Rates
 #9 Can Filler
 (hour 41 and 33 hour averages)

Results (continued)

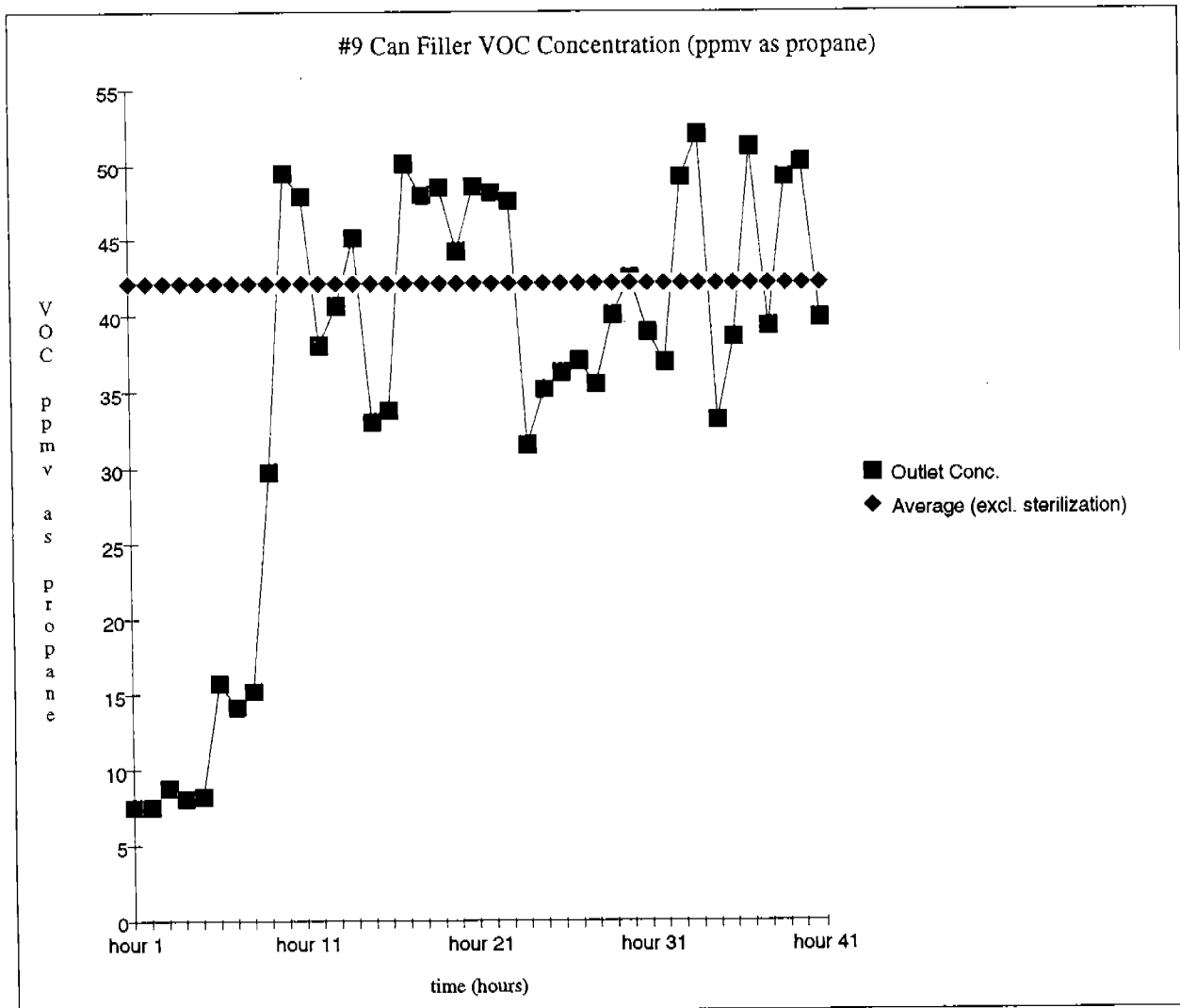


Chart 1 - VOC Concentration
#9 Can Filler

Appendix 1
Testing Parameters

**#3 Bottle Filler
Testing Parameters**

Coors Brewing Company**#3 Bottle Filler Exhaust Vent****12-2-92****EPA Methods 1-4 : Determination of Volumetric Flow Rate and Molecular Weight**

<u>Field Data</u>	Run #1	Run #2	Run #3	Averages
sample volume (ft3)	31.480	43.288	47.742	40.837
sampling time (minutes)	32	40	40	37
stack temp. (oF)	72	69	68	70
meter temp. (oF)	84	93	94	90
barometric pressure (mbar)	833	833	833	833
barometric pressure (" Hg)	24.604	24.604	24.604	24.604
static press. (in. water)	0.07	0.08	0.07	0.07
moisture (grams)	7.5	7.0	4.0	6.2
oxygen (%)	20.9	20.9	20.9	20.9
carbon dioxide (%)	0.0	0.0	0.0	0.0
delta H	3.00	3.10	3.50	3.20
(delta p)^1/2	0.1885	0.1867	0.1900	0.1884
meter box Y	1.0389	1.0389	1.0389	1.0389
delta H@	1.683	1.683	1.683	1.683
pitot tube constant	0.84	0.84	0.84	0.84
stack diameter (inches)	22.0	22.0	22.0	22.0
<u>Calculations</u>	Run #1	Run #2	Run #3	Averages
sample volume (dscf)	26.329	35.627	39.268	33.741
moisture volume (scf)	0.353	0.329	0.188	0.290
moisture content (%/100)	0.0132	0.0092	0.0048	0.0091
molecular weight (dry)	28.836	28.836	28.836	28.836
molecular weight (actual)	28.693	28.737	28.784	28.738
gas velocity (ft/sec)	11.7	11.6	11.8	11.7
gas flow (acfm)	1861	1837	1866	1855
gas flow (dscfm)	1499	1494	1528	1507

Coors Brewing Company

#3 Bottle Filler Inlet #1

12-2-92

EPA Methods 1-4 : Determination of Volumetric Flow Rate and Molecular Weight

<u>Field Data</u>	Run #1	Run #2	Run #3	Averages
stack temp. (oF)	65	64	64	64
barometric pressure (mbar)	833	833	829	832
barometric pressure (" Hg)	24.604	24.604	24.485	24.564
static press. (in. water)	3.80	3.80	3.90	3.83
oxygen (%)	20.9	20.9	20.9	20.9
carbon dioxide (%)	0.0	0.0	0.0	0.0
(delta p)^1/2	0.1935	0.2433	0.1988	0.2119
pitot tube constant	0.84	0.84	0.84	0.84
stack diameter (inches)*	24.0	24.0	24.0	24.0
<u>Calculations</u>	Run #1	Run #2	Run #3	Averages
molecular weight (dry)	28.836	28.836	28.836	28.836
gas velocity (ft/sec)	11.9	14.9	12.2	13.0
gas flow (acfm)	2241	2815	2305	2453
gas flow (dscfm)	1874	2359	1923	2052

* - equivalent diameter of a round stack

Coors Brewing Company

#3 Bottle Filler Inlet #2

12-2-92

EPA Methods 1-4 : Determination of Volumetric Flow Rate and Molecular Weight

<u>Field Data</u>	Run #1	Run #2	Run #3	Averages
stack temp. (oF)	70	70	70	70
barometric pressure (mbar)	833	833	829	832
barometric pressure (" Hg)	24.604	24.604	24.485	24.564
static press. (in. water)	1.20	1.40	1.40	1.33
oxygen (%)	20.9	20.9	20.9	20.9
carbon dioxide (%)	0.0	0.0	0.0	0.0
(delta p)^1/2	0.5808	0.5664	0.5846	0.5773
pitot tube constant	0.84	0.84	0.84	0.84
stack diameter (inches)*	13.9	13.9	13.9	13.9
<u>Calculations</u>	Run #1	Run #2	Run #3	Averages
molecular weight (dry)	28.836	28.836	28.836	28.836
gas velocity (ft/sec)	36.0	35.1	36.3	35.8
gas flow (acfm)	2275	2218	2295	2263
gas flow (dscfm)	1871	1825	1879	1858

* - equivalent diameter of a round stack

Coors Brewing Company

#3 Bottle Filler Inlet #3

12-2-92

EPA Methods 1-4 : Determination of Volumetric Flow Rate and Molecular Weight

<u>Field Data</u>	Run #1	Run #2	Run #3	Averages
stack temp. (oF)	69	68	68	68
barometric pressure (mbar)	833	833	829	832
barometric pressure (" Hg)	24.604	24.604	24.485	24.564
static press. (in. water)	1.00	1.00	1.10	1.03
oxygen (%)	20.9	20.9	20.9	20.9
carbon dioxide (%)	0.0	0.0	0.0	0.0
(delta p)^1/2	0.3989	0.5082	0.5777	0.4949
pitot tube constant	0.84	0.84	0.84	0.84
stack diameter (inches)*	16.6	16.6	16.6	16.6
<u>Calculations</u>	Run #1	Run #2	Run #3	Averages
molecular weight (dry)	28.836	28.836	28.836	28.836
gas velocity (ft/sec)	24.7	31.4	35.8	30.6
gas flow (acfm)	2222	2828	3222	2757
gas flow (dscfm)	1829	2333	2646	2269

* - equivalent diameter of a round stack

Coors Brewing Company

#3 Bottle Filler Exhaust Vent

12-2-92

Method 25A : Measurement of Total Organic Concentration Using a Flame
Ionization Analyzer

Strip Chart Data

Run #1

		Zero (%FS)	Span (%FS)	Actual Span (ppm)
Start	09:00	0.0	39.5	40.1
Stop	10:00	0.5	39.0	

point #	%FS VOC	ppm VOC	point #	%FS VOC	ppm VOC
1	41.0	41.9	26	23.0	23.4
2	38.5	39.3	27	23.0	23.4
3	35.0	35.7	28	29.0	29.6
4	28.0	28.5	29	30.5	31.1
5	21.0	21.3	30	31.0	31.6
6	16.5	16.7	31	31.5	32.1
7	14.0	14.1	32	31.0	31.6
8	20.0	20.3	33	31.0	31.6
9	25.0	25.4	34	31.0	31.6
10	23.0	23.4	35	31.0	31.6
11	18.0	18.3	36	30.5	31.1
12	14.5	14.7	37	30.5	31.1
13	14.5	14.7	38	30.5	31.1
14	24.5	24.9	39	30.0	30.6
15	29.5	30.1	40	27.5	28.0
16	31.5	32.1	41	24.0	24.4
17	32.0	32.6	42	28.5	29.0
18	32.0	32.6	43	31.0	31.6
19	32.0	32.6	44	31.0	31.6
20	32.0	32.6	45	29.0	29.6
21	32.0	32.6	46	23.0	23.4
22	33.0	33.7	47	20.5	20.8
23	32.0	32.6	48	26.0	26.5
24	32.0	32.6	49	27.5	28.0
25	29.0	29.6	50	29.0	29.6
averages:	27.2	27.7		28.9	29.5

Drift Cal. Avg. VOC (ppm as propane) 28.6

Coors Brewing Company

#3 Bottle Filler Exhaust Vent

12-2-92

Method 25A : Measurement of Total Organic Concentration Using a Flame

Ionization Analyzer

Strip Chart Data

Run #2

		Zero (%FS)	Span (%FS)	Actual Span (ppm)
Start	11:00	0.0	40.0	40.1
Stop	12:00	0.0	40.5	

point #	%FS VOC	ppm VOC	point #	%FS VOC	ppm VOC
1	31.0	30.9	26	31.0	30.9
2	31.0	30.9	27	31.5	31.4
3	36.0	35.9	28	30.5	30.4
4	33.0	32.9	29	32.5	32.4
5	32.5	32.4	30	33.0	32.9
6	32.5	32.4	31	32.0	31.9
7	32.0	31.9	32	31.5	31.4
8	32.0	31.9	33	32.0	31.9
9	32.0	31.9	34	31.0	30.9
10	32.5	32.4	35	27.5	27.4
11	32.5	32.4	36	25.5	25.4
12	32.0	31.9	37	23.0	22.9
13	31.5	31.4	38	21.5	21.4
14	31.5	31.4	39	23.0	22.9
15	32.0	31.9	40	25.5	25.4
16	31.5	31.4	41	29.0	28.9
17	31.5	31.4	42	30.0	29.9
18	31.5	31.4	43	30.0	29.9
19	31.5	31.4	44	30.0	29.9
20	32.0	31.9	45	30.0	29.9
21	31.5	31.4	46	30.0	29.9
22	30.5	30.4	47	30.0	29.9
23	30.0	29.9	48	31.0	30.9
24	30.5	30.4	49	30.0	29.9
25	30.5	30.4	50	24.5	24.4
averages:	31.8	31.7		29.0	28.9

Drift Cal. Avg. VOC (ppm as propane) 30.3

Coors Brewing Company**#3 Bottle Filler Exhaust Vent**

12-2-92

Method 25A : Measurement of Total Organic Concentration Using a Flame**Ionization Analyzer****Strip Chart Data**

Run #3

		Zero (%FS)	Span (%FS)	Actual Span (ppm)
Start	12:30	0.0	40.5	40.1
Stop	13:30	0.0	41.0	

point #	%FS VOC	ppm VOC	point #	%FS VOC	ppm VOC
1	31.0	30.5	26	33.0	32.5
2	30.5	30.0	27	33.0	32.5
3	30.5	30.0	28	32.5	32.0
4	30.5	30.0	29	32.5	32.0
5	31.0	30.5	30	32.5	32.0
6	31.0	30.5	31	32.0	31.5
7	31.5	31.0	32	31.5	31.0
8	30.0	29.5	33	31.5	31.0
9	31.0	30.5	34	31.5	31.0
10	31.5	31.0	35	31.5	31.0
11	31.5	31.0	36	31.0	30.5
12	31.0	30.5	37	30.5	30.0
13	31.0	30.5	38	31.0	30.5
14	30.5	30.0	39	31.5	31.0
15	30.0	29.5	40	31.0	30.5
16	30.0	29.5	41	31.0	30.5
17	30.0	29.5	42	31.0	30.5
18	30.0	29.5	43	31.0	30.5
19	30.5	30.0	44	33.5	33.0
20	31.0	30.5	45	30.0	29.5
21	31.0	30.5	46	30.0	29.5
22	31.0	30.5	47	31.0	30.5
23	30.0	29.5	48	27.0	26.6
24	30.0	29.5	49	21.5	21.2
25	30.0	29.5	50	20.0	19.7
averages:	30.6	30.2		31.6	31.1

Drift Cal. Avg. VOC (ppm as propane) 30.6



**#5 Can Filler
Testing Parameters**

Coors Brewing Company
#5 Can Filler Exhaust Vent

12-2-92

EPA Methods 1-4 : Determination of Volumetric Flow Rate and Molecular Weight

<u>Field Data</u>	Run #1	Run #2	Run #3	Averages
sample volume (ft3)	56.039	30.818	33.329	40.062
sampling time (minutes)	50	30	30	37
stack temp. (oF)	68	68	68	68
meter temp. (oF)	82	88	88	86
barometric pressure (mbar)	828	828	827	828
barometric pressure (" Hg)	24.456	24.456	24.426	24.446
static press. (in. water)	-2.60	-2.80	-2.40	-2.60
moisture (grams)	9.0	5.0	6.0	6.7
oxygen (%)	20.9	20.9	20.9	20.9
carbon dioxide (%)	0.0	0.0	0.0	0.0
delta H	3.50	3.50	3.50	3.50
(delta p)^1/2	0.8462	0.8428	0.8145	0.8345
meter box Y	1.0389	1.0389	1.0389	1.0389
delta H@	1.683	1.683	1.683	1.683
pitot tube constant	0.84	0.84	0.84	0.84
stack diameter (inches)	15.0	15.0	15.0	15.0
<u>Calculations</u>	Run #1	Run #2	Run #3	Averages
sample volume (dscf)	46.833	25.473	27.516	33.274
moisture volume (scf)	0.424	0.235	0.282	0.314
moisture content (%/100)	0.0090	0.0092	0.0102	0.0094
molecular weight (dry)	28.836	28.836	28.836	28.836
molecular weight (actual)	28.739	28.737	28.726	28.734
gas velocity (ft/sec)	52.9	52.7	50.9	52.2
gas flow (acfm)	3894	3879	3750	3841
gas flow (dscfm)	3130	3116	3009	3085

Coors Brewing Company

#5 Can Filler Inlet #1

1-27-93

EPA Methods 1-4 : Determination of Volumetric Flow Rate and Molecular Weight

<u>Field Data</u>	Run #1	Run #2	Run #3	Averages
stack temp. (oF)	72	73	73	73
barometric pressure (mbar)	837	838	838	838
barometric pressure (" Hg)	24.722	24.751	24.751	24.741
static press. (in. water)	0.29	0.34	0.32	0.32
oxygen (%)	20.9	20.9	20.9	20.9
carbon dioxide (%)	0.0	0.0	0.0	0.0
(delta p)^1/2	0.5268	0.5321	0.5224	0.5271
pitot tube constant	0.84	0.84	0.84	0.84
stack diameter (inches)*	15.5	15.5	15.5	15.5
<u>Calculations</u>	Run #1	Run #2	Run #3	Averages
molecular weight (dry)	28.836	28.836	28.836	28.836
gas velocity (ft/sec)	32.7	33.0	32.4	32.7
gas flow (acfm)	2568	2595	2548	2570
gas flow (dscfm)	2108	2129	2090	2109

* - equivalent diameter of a round stack

Coors Brewing Company

#5 Can Filler Inlet #2

1-27-93

EPA Methods 1-4 : Determination of Volumetric Flow Rate and Molecular Weight

<u>Field Data</u>	Run #1	Run #2	Run #3	Averages
stack temp. (oF)	78	77	78	78
barometric pressure (mbar)	837	838	838	838
barometric pressure (" Hg)	24.722	24.751	24.751	24.741
static press. (in. water)	1.30	1.30	1.30	1.30
oxygen (%)	20.9	20.9	20.9	20.9
carbon dioxide (%)	0.0	0.0	0.0	0.0
(delta p)^1/2	0.3014	0.3520	0.2909	0.3148
pitot tube constant	0.84	0.84	0.84	0.84
stack diameter (inches)*	22.9	22.9	22.9	22.9
<u>Calculations</u>	Run #1	Run #2	Run #3	Averages
molecular weight (dry)	28.836	28.836	28.836	28.836
gas velocity (ft/sec)	18.8	21.9	18.1	19.6
gas flow (acfm)	3212	3746	3099	3352
gas flow (dscfm)	2615	3059	2526	2733

* - equivalent diameter of a round stack

Coors Brewing Company
 #5 Can Filler Exhaust Vent
 12-2-92

Method 25A : Measurement of Total Organic Concentration Using a Flame
 Ionization Analyzer

Strip Chart Data

Run #1

		Zero (%FS)	Span (%FS)	Actual Span (ppm)
Start	17:00	0.0	45.5	91.3
Stop	18:00	0.0	45.0	

point #	%FS VOC	ppm VOC	point #	%FS VOC	ppm VOC
1	49.5	99.9	26	45.0	90.8
2	51.5	103.9	27	48.0	96.8
3	51.5	103.9	28	47.0	94.8
4	51.0	102.9	29	41.5	83.7
5	51.0	102.9	30	43.0	86.8
6	51.5	103.9	31	46.5	93.8
7	51.0	102.9	32	47.5	95.8
8	51.0	102.9	33	48.0	96.8
9	50.0	100.9	34	47.0	94.8
10	50.0	100.9	35	47.5	95.8
11	50.0	100.9	36	48.5	97.9
12	51.0	102.9	37	48.0	96.8
13	50.5	101.9	38	44.0	88.8
14	50.5	101.9	39	41.0	82.7
15	49.5	99.9	40	42.5	85.8
16	50.0	100.9	41	44.5	89.8
17	49.5	99.9	42	37.0	74.7
18	50.0	100.9	43	29.0	58.5
19	50.0	100.9	44	24.5	49.4
20	49.5	99.9	45	32.0	64.6
21	49.5	99.9	46	40.0	80.7
22	50.0	100.9	47	46.5	93.8
23	43.0	86.8	48	48.0	96.8
24	38.0	76.7	49	48.5	97.9
25	41.5	83.7	50	48.0	96.8
averages:	49.2	99.3		43.3	87.4

Drift Cal. Avg. VOC (ppm as propane) 93.4

Coors Brewing Company
 #5 Can Filler Exhaust Vent
 12-2-92

Method 25A : Measurement of Total Organic Concentration Using a Flame
 Ionization Analyzer

Strip Chart Data

Run #2

		Zero (%FS)	Span (%FS)	Actual Span (ppm)
Start	18:06	0.0	45.0	91.3
Stop	19:06	0.0	45.0	

point #	%FS VOC	ppm VOC	point #	%FS VOC	ppm VOC
1	49.5	100.4	26	38.0	77.1
2	49.5	100.4	27	36.5	74.1
3	49.0	99.4	28	39.5	80.1
4	49.0	99.4	29	42.0	85.2
5	44.0	89.3	30	44.0	89.3
6	25.0	50.7	31	45.0	91.3
7	18.5	37.5	32	46.0	93.3
8	23.0	46.7	33	47.5	96.4
9	32.5	65.9	34	47.5	96.4
10	40.0	81.2	35	48.5	98.4
11	44.0	89.3	36	49.0	99.4
12	44.5	90.3	37	48.5	98.4
13	45.5	92.3	38	49.5	100.4
14	47.0	95.4	39	49.0	99.4
15	44.0	89.3	40	49.0	99.4
16	43.5	88.3	41	49.0	99.4
17	39.5	80.1	42	51.0	103.5
18	41.0	83.2	43	50.5	102.5
19	42.0	85.2	44	49.0	99.4
20	43.0	87.2	45	50.0	101.4
21	41.0	83.2	46	54.5	110.6
22	34.0	69.0	47	52.0	105.5
23	28.5	57.8	48	45.0	91.3
24	26.5	53.8	49	45.0	91.3
25	33.0	67.0	50	46.0	93.3
averages:	39.1	79.3		46.9	95.1

Drift Cal. Avg. VOC (ppm as propane) 87.2

Coors Brewing Company

#5 Can Filler Exhaust Vent

12-2-92

Method 25A : Measurement of Total Organic Concentration Using a Flame

Ionization Analyzer

Strip Chart Data

Run #3

		Zero (%FS)	Span (%FS)	Actual Span (ppm)
Start	19:10	0.0	45.0	91.3
Stop	20:10	0.0	45.5	

point #	%FS VOC	ppm VOC	point #	%FS VOC	ppm VOC
1	18.5	37.3	26	50.0	100.9
2	18.0	36.3	27	51.0	102.9
3	16.5	33.3	28	50.0	100.9
4	14.0	28.2	29	45.0	90.8
5	13.5	27.2	30	47.0	94.8
6	23.5	47.4	31	49.5	99.9
7	27.5	55.5	32	50.5	101.9
8	28.5	57.5	33	52.0	104.9
9	28.5	57.5	34	51.5	103.9
10	32.0	64.6	35	51.0	102.9
11	39.5	79.7	36	50.5	101.9
12	44.0	88.8	37	50.5	101.9
13	46.5	93.8	38	48.0	96.8
14	49.0	98.9	39	42.5	85.8
15	50.5	101.9	40	45.5	91.8
16	50.0	100.9	41	45.0	90.8
17	50.5	101.9	42	46.5	93.8
18	49.0	98.9	43	46.0	92.8
19	42.0	84.7	44	46.0	92.8
20	38.5	77.7	45	47.5	95.8
21	39.5	79.7	46	48.5	97.9
22	42.5	85.8	47	49.0	98.9
23	47.0	94.8	48	49.5	99.9
24	49.0	98.9	49	49.0	98.9
25	50.0	100.9	50	49.5	99.9
averages:	36.3	73.3		48.4	97.7

Drift Cal. Avg. VOC (ppm as propane) 85.5



**#6 Can Filler
Testing Parameters**

Coors Brewing Company
#6 Can Filler Exhaust Vent
12-16-92

EPA Methods 1-4 : Determination of Volumetric Flow Rate and Molecular Weight

<u>Field Data</u>	Run #1	Run #2	Run #3	Averages
sample volume (ft3)	28.974	31.148	35.014	31.712
sampling time (minutes)	30	30	30	30
stack temp. (oF)	68	68	72	69
meter temp. (oF)	81	91	85	86
barometric pressure (mbar)	836	834	836	835
barometric pressure (" Hg)	24.692	24.633	24.692	24.672
static press. (in. water)	-0.49	-0.48	-0.47	-0.48
moisture (grams)	8.0	4.5	7.0	6.5
oxygen (%)	20.9	20.9	20.9	20.9
carbon dioxide (%)	0.0	0.0	0.0	0.0
delta H	3.00	3.00	3.50	3.17
(delta p)^1/2	0.3817	0.3805	0.3659	0.3760
meter box Y	1.0389	1.0389	1.0389	1.0389
delta H@	1.683	1.683	1.683	1.683
pitot tube constant	0.84	0.84	0.84	0.84
stack diameter (inches)	17.5	17.5	17.5	17.5
<u>Calculations</u>	Run #1	Run #2	Run #3	Averages
sample volume (dscf)	24.455	25.751	29.379	26.528
moisture volume (scf)	0.377	0.212	0.329	0.306
moisture content (%/100)	0.0152	0.0082	0.0111	0.0115
molecular weight (dry)	28.836	28.836	28.836	28.836
molecular weight (actual)	28.672	28.748	28.716	28.712
gas velocity (ft/sec)	23.7	23.6	22.8	23.4
gas flow (acfm)	2374	2366	2283	2341
gas flow (dscfm)	1927	1930	1847	1901

Coors Brewing Company

#6 Can Filler Inlet #1

12-16-92

EPA Methods 1-4 : Determination of Volumetric Flow Rate and Molecular Weight

<u>Field Data</u>	Run #1	Run #2	Run #3	Averages
stack temp. (oF)	74	74	74	74
barometric pressure (mbar)	836	834	836	835
barometric pressure (" Hg)	24.692	24.633	24.692	24.672
static press. (in. water)	0.28	0.27	0.27	0.27
oxygen (%)	20.9	20.9	20.9	20.9
carbon dioxide (%)	0.0	0.0	0.0	0.0
(delta p) ^{1/2}	0.3807	0.1680	0.1041	0.2176
pitot tube constant	0.84	0.84	0.84	0.84
stack diameter (inches)*	24.4	24.4	24.4	24.4
<u>Calculations</u>	Run #1	Run #2	Run #3	Averages
molecular weight (dry)	28.836	28.836	28.836	28.836
gas velocity (ft/sec)	23.7	10.5	6.5	13.5
gas flow (acfm)	4611	2037	1261	2636
gas flow (dscfm)	3766	1660	1030	2152

* - equivalent diameter of a round stack

Coors Brewing Company

#6 Can Filler Inlet #2

12-16-92

EPA Methods 1-4 : Determination of Volumetric Flow Rate and Molecular Weight

<u>Field Data</u>	Run #1	Run #2	Run #3	Averages
stack temp. (oF)	71	71	71	71
barometric pressure (mbar)	836	834	836	835
barometric pressure (" Hg)	24.692	24.633	24.692	24.672
static press. (in. water)	0.94	0.92	1.80	1.22
oxygen (%)	20.9	20.9	20.9	20.9
carbon dioxide (%)	0.0	0.0	0.0	0.0
(delta p)^1/2	0.3784	0.3454	0.4896	0.4045
pitot tube constant	0.84	0.84	0.84	0.84
stack diameter (inches)*	16.9	16.9	16.9	16.9
<u>Calculations</u>	Run #1	Run #2	Run #3	Averages
molecular weight (dry)	28.836	28.836	28.836	28.836
gas velocity (ft/sec)	23.4	21.4	30.3	25.0
gas flow (acfm)	2190	2002	2830	2341
gas flow (dscfm)	1803	1643	2335	1927

* - equivalent diameter of a round stack

Coors Brewing Company
 #6 Can Filler Exhaust Vent
 12-16-92

Method 25A : Measurement of Total Organic Concentration Using a Flame
 Ionization Analyzer

Strip Chart Data

Run #1

		Zero (%FS)		Span (%FS)		Actual Span (ppm)			
Start	10:00	0.0	46.0			91.3			
Stop	11:00	0.0	44.0						
point #	%FS VOC	ppm VOC	point #	%FS VOC	ppm VOC	point #	%FS VOC	ppm VOC	
1	46.0	93.3	21	61.0	123.8	41	69.0	140.0	
2	43.0	87.2	22	62.0	125.8	42	54.0	109.6	
3	31.0	62.9	23	60.0	121.7	43	62.0	125.8	
4	25.0	50.7	24	59.0	119.7	44	65.0	131.9	
5	38.0	77.1	25	47.0	95.4	45	68.0	138.0	
6	48.0	97.4	26	33.0	67.0	46	66.0	133.9	
7	54.0	109.6	27	25.0	50.7	47	48.0	97.4	
8	57.0	115.6	28	27.0	54.8	48	36.0	73.0	
9	60.0	121.7	29	42.0	85.2	49	42.0	85.2	
10	62.0	125.8	30	49.0	99.4	50	58.0	117.7	
11	62.0	125.8	31	46.0	93.3	51	62.0	125.8	
12	62.0	125.8	32	52.0	105.5	52	60.0	121.7	
13	63.0	127.8	33	57.0	115.6	53	53.0	107.5	
14	63.0	127.8	34	59.0	119.7	54	61.0	123.8	
15	62.0	125.8	35	58.0	117.7	55	66.0	133.9	
16	63.0	127.8	36	57.0	115.6	56	68.0	138.0	
17	62.0	125.8	37	58.0	117.7	57	69.0	140.0	
18	62.0	125.8	38	64.0	129.8	58	69.0	140.0	
19	63.0	127.8	39	68.0	138.0	59	70.0	142.0	
20	62.0	125.8	40	69.0	140.0	60	69.0	140.0	
averages:	54.4	110.4		52.6	106.8		60.8	123.3	

Drift Cal. Avg. VOC (ppm as propane)

113.5

Coors Brewing Company
 #6 Can Filler Exhaust Vent
 12-16-92

Method 25A : Measurement of Total Organic Concentration Using a Flame
 Ionization Analyzer

Strip Chart Data

Run #2

		Zero (%FS)		Span (%FS)		Actual Span (ppm)			
Start	11:30	0.0		46.0		91.3			
Stop	12:30	0.0		44.0					
point #	%FS VOC	ppm VOC	point #	%FS VOC	ppm VOC	point #	%FS VOC	ppm VOC	
1	51.0	103.5	21	65.0	131.9	41	61.0	123.8	
2	56.0	113.6	22	69.0	140.0	42	57.0	115.6	
3	58.0	117.7	23	70.0	142.0	43	36.0	73.0	
4	52.0	105.5	24	70.0	142.0	44	28.0	56.8	
5	56.0	113.6	25	70.0	142.0	45	44.0	89.3	
6	58.0	117.7	26	68.0	138.0	46	56.0	113.6	
7	59.0	119.7	27	70.0	142.0	47	59.0	119.7	
8	59.0	119.7	28	70.0	142.0	48	54.0	109.6	
9	61.0	123.8	29	70.0	142.0	49	53.0	107.5	
10	61.0	123.8	30	68.0	138.0	50	64.0	129.8	
11	54.0	109.6	31	62.0	125.8	51	67.0	135.9	
12	40.0	81.2	32	52.0	105.5	52	66.0	133.9	
13	30.0	60.9	33	59.0	119.7	53	42.0	85.2	
14	24.0	48.7	34	64.0	129.8	54	32.0	64.9	
15	29.0	58.8	35	66.0	133.9	55	34.0	69.0	
16	42.0	85.2	36	66.0	133.9	56	49.0	99.4	
17	41.0	83.2	37	60.0	121.7	57	56.0	113.6	
18	50.0	101.4	38	38.0	77.1	58	61.0	123.8	
19	55.0	111.6	39	39.0	79.1	59	63.0	127.8	
20	57.0	115.6	40	51.0	103.5	60	65.0	131.9	
averages:	49.6	100.7		62.4	126.5		52.4	106.2	

Drift Cal. Avg. VOC (ppm as propane)

111.1

Coors Brewing Company
#6 Can Filler Exhaust Vent

12-16-92

Method 25A : Measurement of Total Organic Concentration Using a Flame
Ionization Analyzer

Strip Chart Data

Run #3

		Zero (%FS)	Span (%FS)	Actual Span (ppm)
Start	13:00	0.0	46.0	91.3
Stop	14:00	1.0	47.0	

point #	%FS VOC	ppm VOC	point #	%FS VOC	ppm VOC	point #	%FS VOC	ppm VOC
1	61.0	120.1	21	61.0	120.1	41	43.0	84.4
2	40.0	78.4	22	61.0	120.1	42	55.0	108.2
3	40.0	78.4	23	61.0	120.1	43	62.0	122.1
4	50.0	98.2	24	49.0	96.3	44	65.0	128.0
5	56.0	110.2	25	38.0	74.4	45	67.0	132.0
6	59.0	116.1	26	30.0	58.6	46	66.0	130.0
7	47.0	92.3	27	24.0	46.6	47	67.0	132.0
8	37.0	72.4	28	42.0	82.4	48	66.0	130.0
9	36.0	70.5	29	52.0	102.2	49	66.0	130.0
10	54.0	106.2	30	57.0	112.1	50	66.0	130.0
11	57.0	112.1	31	60.0	118.1	51	66.0	130.0
12	60.0	118.1	32	61.0	120.1	52	65.0	128.0
13	61.0	120.1	33	61.0	120.1	53	66.0	130.0
14	60.0	118.1	34	61.0	120.1	54	66.0	130.0
15	60.0	118.1	35	62.0	122.1	55	66.0	130.0
16	61.0	120.1	36	61.0	120.1	56	67.0	132.0
17	60.0	118.1	37	61.0	120.1	57	67.0	132.0
18	60.0	118.1	38	61.0	120.1	58	56.0	110.2
19	61.0	120.1	39	60.0	118.1	59	49.0	96.3
20	61.0	120.1	40	57.0	112.1	60	48.0	94.3
averages:	54.0	106.3		54.0	106.2		62.0	122.0

Drift Cal. Avg. VOC (ppm as propane)

111.5

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**#9 Can Filler
Testing Parameters**

Coors Brewing Company
#9 Can Filler Exhaust Vent

12-3-92 through 12-5-92

EPA Methods 1-4 : Determination of Volumetric Flow Rate and Molecular Weight

<u>Field Data</u>	Run #1	Run #2	Run #3	Run #4	Run #5	Averages
sample volume (ft3)	41.325	31.521	32.206	32.111	31.678	33.768
sampling time (minutes)	40	30	30	30	30	32
stack temp. (oF)	70	70	70	71	71	70
meter temp. (oF)	91	84	82	83	84	85
barometric pressure (mbar)	828	827	829	828	827	828
barometric pressure (" Hg)	24.456	24.426	24.485	24.456	24.426	24.450
static press. (in. water)	-3.00	-3.00	-2.90	-3.00	-3.00	-2.98
moisture (grams)	4.0	3.0	3.5	2.5	4.0	3.4
oxygen (%)	20.9	20.9	20.9	20.9	20.9	20.9
carbon dioxide (%)	0.0	0.0	0.0	0.0	0.0	0.0
delta H	3.50	3.50	3.50	3.50	3.50	3.50
(delta p)^1/2	0.5894	0.5988	0.5967	0.5990	0.6030	0.5974
meter box Y	1.0389	1.0389	1.0389	1.0389	1.0389	1.0389
delta H@	1.683	1.683	1.683	1.683	1.683	1.683
pitot tube constant	0.84	0.84	0.84	0.84	0.84	0.84
stack diameter (inches)	15.5	15.5	15.5	15.5	15.5	15.5
<u>Calculations</u>	Run #1	Run #2	Run #3	Run #4	Run #5	Averages
sample volume (dscf)	33.972	26.214	26.947	26.786	26.345	28.053
moisture volume (scf)	0.188	0.141	0.165	0.118	0.188	0.160
moisture content (%/100)	0.0055	0.0054	0.0061	0.0044	0.0071	0.0057
molecular weight (dry)	28.836	28.836	28.836	28.836	28.836	28.836
molecular weight (actual)	28.776	28.778	28.770	28.789	28.759	28.774
gas velocity (ft/sec)	36.9	37.5	37.3	37.5	37.8	37.4
gas flow (acfm)	2901	2949	2935	2951	2974	2942
gas flow (dscfm)	2328	2364	2358	2366	2375	2359

Coors Brewing Company

#9 Can Filler Inlet #1

12-3-92 through 12-5-92

EPA Methods 1-4 : Determination of Volumetric Flow Rate and Molecular Weight

<u>Field Data</u>	Run #1	Run #2	Run #3	Run #4	Run #5	Averages
stack temp. (oF)	76	75	76	74	74	75
barometric pressure (mbar)	828	827	829	828	827	828
barometric pressure (" Hg)	24.456	24.426	24.485	24.456	24.426	24.450
static press. (in. water)	1.20	1.90	1.40	1.40	1.30	1.44
oxygen (%)	20.9	20.9	20.9	20.9	20.9	20.9
carbon dioxide (%)	0.0	0.0	0.0	0.0	0.0	0.0
(delta p) ^{1/2}	0.7367	0.8922	0.8057	0.8063	0.7857	0.8053
pitot tube constant	0.84	0.84	0.84	0.84	0.84	0.84
stack diameter (inches)*	21.9	21.9	21.9	21.9	21.9	21.9
<u>Calculations</u>	Run #1	Run #2	Run #3	Run #4	Run #5	Averages
molecular weight (dry)	28.836	28.836	28.836	28.836	28.836	28.836
gas velocity (ft/sec)	46.0	55.7	50.3	50.3	49.0	50.3
gas flow (acfm)	7226	8740	7896	7892	7696	7890
gas flow (dscfm)	5840	7083	6393	6406	6238	6392

* - equivalent diameter of a round stack

Coors Brewing Company

#9 Can Filler Inlet #2

12-3-92 through 12-5-92

EPA Methods 1-4 : Determination of Volumetric Flow Rate and Molecular Weight

<u>Field Data</u>	Run #1	Run #2	Run #3	Run #4	Run #5	Averages
stack temp. (oF)	76	76	72	71	72	73
barometric pressure (mbar)	828	827	829	828	827	828
barometric pressure (" Hg)	24.456	24.426	24.485	24.456	24.426	24.450
static press. (in. water)	-0.41	-0.40	-0.29	-0.40	-0.35	-0.37
oxygen (%)	20.9	20.9	20.9	20.9	20.9	20.9
carbon dioxide (%)	0.0	0.0	0.0	0.0	0.0	0.0
(delta p) ^{1/2} (center line)**	0.9722	1.0110	1.1221	0.9689	0.9743	1.0097
(delta p) ^{1/2} (corrected)**	0.6592	0.6855	0.7608	0.6569	0.6606	0.6846
pitot tube constant	0.84	0.84	0.84	0.84	0.84	0.84
stack diameter (inches)*	14.5	14.5	14.5	14.5	14.5	14.5
<u>Calculations</u>	Run #1	Run #2	Run #3	Run #4	Run #5	Averages
molecular weight (dry)	28.836	28.836	28.836	28.836	28.836	28.836
gas velocity (ft/sec)	41.3	43.0	47.4	41.0	41.2	42.8
gas flow (acfm)	2841	2956	3265	2818	2838	2944
gas flow (dscfm)	2285	2375	2650	2288	2298	2379

* - equivalent diameter of a round stack

** - When the original flow measurements were taken, only the center port was accessible.

Subsequent flow measurements of all ports were used to develop an empirical constant (0.678) to determine total duct flow from the center port differential pressure measurements.

Coors Brewing Company

#9 Can Filler Exhaust Vent

12-3-92

Method 25A : Measurement of Total Organic Concentration Using a Flame

Ionization Analyzer

Strip Chart Data

Hours 1 - 2

		Zero (%FS)	Span (%FS)	Actual Span (ppm)
Start	07:30	0.0	40.0	40.1
Stop	09:30	0.0	39.0	

point #	%FS VOC	ppm VOC	point #	%FS VOC	ppm VOC
1	8.0	8.1	21	7.0	7.1
2	8.0	8.1	22	7.0	7.1
3	8.0	8.1	23	7.0	7.1
4	8.0	8.1	24	6.0	6.1
5	8.0	8.1	25	6.0	6.1
6	8.0	8.1	26	6.0	6.1
7	8.0	8.1	27	6.0	6.1
8	8.0	8.1	28	6.0	6.1
9	8.0	8.1	29	7.0	7.1
10	8.0	8.1	30	7.0	7.1
11	7.0	7.1	31	8.0	8.1
12	7.0	7.1	32	8.0	8.1
13	7.0	7.1	33	8.0	8.1
14	7.0	7.1	34	8.0	8.1
15	7.0	7.1	35	8.0	8.1
16	7.0	7.1	36	8.0	8.1
17	7.0	7.1	37	9.0	9.1
18	7.0	7.1	38	9.0	9.1
19	7.0	7.1	39	9.0	9.1
20	7.0	7.1	40	9.0	9.1
averages:	7.5	7.6		7.5	7.6

Drift Cal. Avg. VOC (ppm as propane) 7.6

Coors Brewing Company

#9 Can Filler Exhaust Vent

12-3-92

Method 25A : Measurement of Total Organic Concentration Using a Flame

Ionization Analyzer

Strip Chart Data

Hours 3 - 4

		Zero (%FS)	Span (%FS)	Actual Span (ppm)
Start	09:30	0.0	40.0	40.1
Stop	11:30	0.0	39.0	

point #	%FS VOC	ppm VOC	point #	%FS VOC	ppm VOC
1	9.0	9.1	21	8.0	8.1
2	9.0	9.1	22	8.0	8.1
3	9.0	9.1	23	8.0	8.1
4	9.0	9.1	24	8.0	8.1
5	9.0	9.1	25	8.0	8.1
6	9.0	9.1	26	8.0	8.1
7	9.0	9.1	27	8.0	8.1
8	9.0	9.1	28	8.0	8.1
9	9.0	9.1	29	8.0	8.1
10	9.0	9.1	30	8.0	8.1
11	9.0	9.1	31	8.0	8.1
12	9.0	9.1	32	9.0	9.1
13	9.0	9.1	33	9.0	9.1
14	9.0	9.1	34	9.0	9.1
15	9.0	9.1	35	8.0	8.1
16	9.0	9.1	36	8.0	8.1
17	8.0	8.1	37	8.0	8.1
18	8.0	8.1	38	8.0	8.1
19	8.0	8.1	39	7.0	7.1
20	8.0	8.1	40	8.0	8.1
averages:	8.8	8.9		8.1	8.2

Drift Cal. Avg. VOC (ppm as propane) 8.6

Coors Brewing Company
 #9 Can Filler Exhaust Vent
 12-3-92

Method 25A : Measurement of Total Organic Concentration Using a Flame
 Ionization Analyzer

Strip Chart Data

Hours 5 - 6

		Zero (%FS)	Span (%FS)	Actual Span (ppm)
Start	11:30	0.0	40.0	40.1
Stop	13:30	0.0	41.0	

point #	%FS VOC	ppm VOC	point #	%FS VOC	ppm VOC
1	8.0	7.9	21	12.0	11.9
2	8.0	7.9	22	13.0	12.9
3	8.0	7.9	23	16.0	15.8
4	8.0	7.9	24	24.0	23.8
5	8.0	7.9	25	20.0	19.8
6	9.0	8.9	26	18.0	17.8
7	9.0	8.9	27	17.0	16.8
8	9.0	8.9	28	18.0	17.8
9	8.0	7.9	29	16.0	15.8
10	8.0	7.9	30	16.0	15.8
11	8.0	7.9	31	17.0	16.8
12	8.0	7.9	32	17.0	16.8
13	8.0	7.9	33	15.0	14.9
14	8.0	7.9	34	14.0	13.9
15	8.0	7.9	35	13.0	12.9
16	8.0	7.9	36	12.0	11.9
17	8.0	7.9	37	12.0	11.9
18	8.0	7.9	38	13.0	12.9
19	9.0	8.9	39	16.0	15.8
20	11.0	10.9	40	20.0	19.8
averages:	8.3	8.3		15.9	15.8

Drift Cal. Avg. VOC (ppm as propane) 12.0

Coors Brewing Company

#9 Can Filler Exhaust Vent

12-3-92

Method 25A : Measurement of Total Organic Concentration Using a Flame
Ionization Analyzer

Strip Chart Data

Hours 7 - 8

		Zero (%FS)	Span (%FS)	Actual Span (ppm)
Start	13:30	0.0	40.0	40.1
Stop	15:30	0.0	41.0	

point #	%FS VOC	ppm VOC	point #	%FS VOC	ppm VOC
1	18.0	17.8	21	13.0	12.9
2	18.0	17.8	22	15.0	14.9
3	17.0	16.8	23	15.0	14.9
4	17.0	16.8	24	13.0	12.9
5	16.0	15.8	25	12.0	11.9
6	16.0	15.8	26	12.0	11.9
7	16.0	15.8	27	12.0	11.9
8	15.0	14.9	28	12.0	11.9
9	14.0	13.9	29	11.0	10.9
10	13.0	12.9	30	11.0	10.9
11	13.0	12.9	31	10.0	9.9
12	12.0	11.9	32	10.0	9.9
13	12.0	11.9	33	10.0	9.9
14	13.0	12.9	34	16.0	15.8
15	13.0	12.9	35	15.0	14.9
16	13.0	12.9	36	19.0	18.8
17	12.0	11.9	37	24.0	23.8
18	13.0	12.9	38	26.0	25.7
19	13.0	12.9	39	27.0	26.7
20	13.0	12.9	40	27.0	26.7
averages:	14.3	14.2		15.5	15.3

Drift Cal. Avg. VOC (ppm as propane) 14.8

Coors Brewing Company

#9 Can Filler Exhaust Vent

12-3-92

Method 25A : Measurement of Total Organic Concentration Using a Flame

Ionization Analyzer

Strip Chart Data

Hours 9 - 10

		Zero (%FS)	Span (%FS)	Actual Span (ppm)
Start	15:30	0.0	41.0	40.1
Stop	17:30	0.0	41.0	

point #	%FS VOC	ppm VOC	point #	%FS VOC	ppm VOC
1	28.0	27.4	21	48.0	46.9
2	26.0	25.4	22	50.0	48.9
3	25.0	24.5	23	50.0	48.9
4	25.0	24.5	24	49.0	47.9
5	25.0	24.5	25	54.0	52.8
6	23.0	22.5	26	55.0	53.8
7	25.0	24.5	27	50.0	48.9
8	20.0	19.6	28	52.0	50.9
9	16.0	15.6	29	50.0	48.9
10	13.0	12.7	30	52.0	50.9
11	13.0	12.7	31	49.0	47.9
12	22.0	21.5	32	52.0	50.9
13	calibrate	calibrate	33	51.0	49.9
14	33.0	32.3	34	52.0	50.9
15	48.0	46.9	35	50.0	48.9
16	52.0	50.9	36	50.0	48.9
17	50.0	48.9	37	50.0	48.9
18	50.0	48.9	38	47.0	46.0
19	39.0	38.1	39	51.0	49.9
20	45.0	44.0	40	51.0	49.9
averages:	30.4	29.8		50.6	49.5

Drift Cal. Avg. VOC (ppm as propane) 39.6

Coors Brewing Company
#9 Can Filler Exhaust Vent

12-3-92

**Method 25A : Measurement of Total Organic Concentration Using a Flame
 Ionization Analyzer**

Strip Chart Data

Hours 11 - 12

		Zero (%FS)	Span (%FS)	Actual Span (ppm)
Start	17:30	0.0	41.0	40.1
Stop	19:30	0.0	41.0	

point #	%FS VOC	ppm VOC	point #	%FS VOC	ppm VOC
1	50.0	48.9	21	48.0	46.9
2	50.0	48.9	22	48.0	46.9
3	50.0	48.9	23	48.0	46.9
4	50.0	48.9	24	50.0	48.9
5	54.0	52.8	25	39.0	38.1
6	50.0	48.9	26	35.0	34.2
7	51.0	49.9	27	44.0	43.0
8	51.0	49.9	28	52.0	50.9
9	50.0	48.9	29	51.0	49.9
10	50.0	48.9	30	50.0	48.9
11	49.0	47.9	31	46.0	45.0
12	53.0	51.8	32	49.0	47.9
13	50.0	48.9	33	51.0	49.9
14	49.0	47.9	34	52.0	50.9
15	50.0	48.9	35	45.0	44.0
16	48.0	46.9	36	21.0	20.5
17	50.0	48.9	37	17.0	16.6
18	34.0	33.3	38	14.0	13.7
19	41.0	40.1	39	12.0	11.7
20	49.0	47.9	40	8.0	7.8
averages:	49.0	47.9		39.0	38.1

Drift Cal. Avg. VOC (ppm as propane) 43.0

Coors Brewing Company
#9 Can Filler Exhaust Vent

12-3-92

Method 25A : Measurement of Total Organic Concentration Using a Flame Ionization Analyzer

Strip Chart Data

Hours 13 - 14

		Zero (%FS)	Span (%FS)	Actual Span (ppm)
Start	19:30	0.0	41.0	40.1
Stop	21:30	0.0	41.0	

point #	%FS VOC	ppm VOC	point #	%FS VOC	ppm VOC
1	5.0	4.9	21	49.0	47.9
2	5.0	4.9	22	49.0	47.9
3	22.0	21.5	23	48.0	46.9
4	42.0	41.1	24	54.0	52.8
5	41.0	40.1	25	51.0	49.9
6	45.0	44.0	26	53.0	51.8
7	50.0	48.9	27	46.0	45.0
8	50.0	48.9	28	43.0	42.1
9	48.0	46.9	29	42.0	41.1
10	51.0	49.9	30	calibrate	calibrate
11	50.0	48.9	31	46.0	45.0
12	47.0	46.0	32	46.0	45.0
13	46.0	45.0	33	46.0	45.0
14	46.0	45.0	34	45.5	44.5
15	49.0	47.9	35	calibrate	calibrate
16	49.0	47.9	36	calibrate	calibrate
17	44.0	43.0	37	43.0	42.1
18	50.0	48.9	38	44.0	43.0
19	50.0	48.9	39	35.0	34.2
20	40.0	39.1	40	44.0	43.0
averages:	41.5	40.6		46.1	45.1

Drift Cal. Avg. VOC (ppm as propane) 42.9

Coors Brewing Company

#9 Can Filler Exhaust Vent

12-3-92

Method 25A : Measurement of Total Organic Concentration Using a Flame

Ionization Analyzer

Strip Chart Data

Hours 15 - 16

		Zero (%FS)	Span (%FS)	Actual Span (ppm)
Start	21:30	0.0	41.0	40.1
Stop	23:30	0.0	42.0	

point #	%FS VOC	ppm VOC	point #	%FS VOC	ppm VOC
1	47.5	45.9	21	11.5	11.1
2	38.0	36.7	22	9.5	9.2
3	19.0	18.4	23	8.0	7.7
4	13.0	12.6	24	8.0	7.7
5	26.0	25.1	25	11.0	10.6
6	42.0	40.6	26	8.0	7.7
7	44.0	42.5	27	32.0	30.9
8	43.0	41.5	28	46.5	44.9
9	47.0	45.4	29	50.0	48.3
10	48.0	46.4	30	49.0	47.3
11	46.0	44.4	31	44.0	42.5
12	44.5	43.0	32	38.0	36.7
13	42.0	40.6	33	23.5	22.7
14	41.5	40.1	34	50.0	48.3
15	48.0	46.4	35	51.0	49.3
16	12.0	11.6	36	52.0	50.2
17	4.5	4.3	37	53.0	51.2
18	23.0	22.2	38	53.0	51.2
19	38.0	36.7	39	47.5	45.9
20	17.0	16.4	40	54.0	52.2
averages:	34.2	33.0		35.0	33.8

Drift Cal. Avg. VOC (ppm as propane) 33.4

Coors Brewing Company
 #9 Can Filler Exhaust Vent
 12-3/4-92

Method 25A : Measurement of Total Organic Concentration Using a Flame
 Ionization Analyzer

Strip Chart Data

Hours 17 - 18

		Zero (%FS)	Span (%FS)	Actual Span (ppm)
Start	23:30	0.0	41.0	40.1
Stop	01:30	0.0	42.0	

point #	%FS VOC	ppm VOC	point #	%FS VOC	ppm VOC
1	44.0	42.5	21	54.0	52.2
2	50.0	48.3	22	53.0	51.2
3	54.0	52.2	23	54.0	52.2
4	54.0	52.2	24	52.5	50.7
5	50.5	48.8	25	51.5	49.8
6	52.0	50.2	26	32.5	31.4
7	51.0	49.3	27	28.5	27.5
8	52.0	50.2	28	48.0	46.4
9	51.0	49.3	29	49.5	47.8
10	51.5	49.8	30	51.0	49.3
11	51.0	49.3	31	51.0	49.3
12	53.0	51.2	32	51.0	49.3
13	53.0	51.2	33	52.0	50.2
14	54.0	52.2	34	53.0	51.2
15	53.0	51.2	35	47.5	45.9
16	52.5	50.7	36	49.5	47.8
17	53.5	51.7	37	53.0	51.2
18	51.0	49.3	38	54.5	52.7
19	53.0	51.2	39	54.5	52.7
20	53.0	51.2	40	53.0	51.2
averages:	51.9	50.1		49.7	48.0

Drift Cal. Avg. VOC (ppm as propane) 49.1

Coors Brewing Company

#9 Can Filler Exhaust Vent

12-4-92

Method 25A : Measurement of Total Organic Concentration Using a Flame
Ionization Analyzer

Strip Chart Data

Hours 19 - 20

		Zero (%FS)	Span (%FS)	Actual Span (ppm)
Start	01:30	0.0	41.0	40.1
Stop	03:30	0.0	42.0	

point #	%FS VOC	ppm VOC	point #	%FS VOC	ppm VOC
1	52.0	50.2	21	52.0	50.2
2	53.5	51.7	22	41.0	39.6
3	52.0	50.2	23	35.0	33.8
4	54.0	52.2	24	25.5	24.6
5	53.5	51.7	25	41.0	39.6
6	49.5	47.8	26	51.0	49.3
7	53.0	51.2	27	49.5	47.8
8	54.0	52.2	28	52.0	50.2
9	53.5	51.7	29	53.0	51.2
10	50.5	48.8	30	52.0	50.2
11	45.0	43.5	31	54.5	52.7
12	49.0	47.3	32	52.0	50.2
13	36.0	34.8	33	42.5	41.1
14	33.0	31.9	34	31.5	30.4
15	51.0	49.3	35	30.0	29.0
16	54.0	52.2	36	45.0	43.5
17	50.0	48.3	37	51.0	49.3
18	52.0	50.2	38	51.0	49.3
19	55.0	53.1	39	53.0	51.2
20	52.5	50.7	40	53.0	51.2
averages:	50.1	48.5		45.8	44.2

Drift Cal. Avg. VOC (ppm as propane) 46.3

Coors Brewing Company
#9 Can Filler Exhaust Vent

12-4-92

Method 25A : Measurement of Total Organic Concentration Using a Flame
Ionization Analyzer

Strip Chart Data

Hours 21 - 22

		Zero (%FS)	Span (%FS)	Actual Span (ppm)
Start	03:30	0.0	41.0	40.1
Stop	05:30	0.0	42.0	

point #	%FS VOC	ppm VOC	point #	%FS VOC	ppm VOC
1	51.5	49.8	21	48.0	46.4
2	51.0	49.3	22	47.0	45.4
3	52.0	50.2	23	46.0	44.4
4	53.0	51.2	24	47.0	45.4
5	52.0	50.2	25	45.0	43.5
6	53.0	51.2	26	49.5	47.8
7	53.0	51.2	27	49.5	47.8
8	53.0	51.2	28	50.0	48.3
9	53.5	51.7	29	51.0	49.3
10	53.0	51.2	30	50.5	48.8
11	47.0	45.4	31	52.0	50.2
12	50.0	48.3	32	51.0	49.3
13	51.0	49.3	33	51.0	49.3
14	49.0	47.3	34	52.0	50.2
15	51.0	49.3	35	52.0	50.2
16	51.0	49.3	36	51.0	49.3
17	52.0	50.2	37	51.0	49.3
18	40.0	38.7	38	53.0	51.2
19	41.0	39.6	39	calibrate	calibrate
20	48.0	46.4	40	51.0	49.3
averages:	50.3	48.6		49.9	48.2

Drift Cal. Avg. VOC (ppm as propane) 48.4

Coors Brewing Company
 #9 Can Filler Exhaust Vent
 12-4-92

Method 25A : Measurement of Total Organic Concentration Using a Flame
 Ionization Analyzer

Strip Chart Data

Hours 23 - 24

		Zero (%FS)	Span (%FS)			Actual Span (ppm)
Start	05:30	0.0	41.0			40.1
Stop	07:30	0.0	41.0			
point #	%FS VOC	ppm VOC	point #	%FS VOC	ppm VOC	
1	52.0	50.9	21	50.0	48.9	
2	55.0	53.8	22	48.0	46.9	
3	54.0	52.8	23	44.0	43.0	
4	54.0	52.8	24	44.0	43.0	
5	35.0	34.2	25	47.0	46.0	
6	26.0	25.4	26	48.0	46.9	
7	46.0	45.0	27	46.0	45.0	
8	46.0	45.0	28	46.0	45.0	
9	50.0	48.9	29	40.0	39.1	
10	50.0	48.9	30	46.0	45.0	
11	52.0	50.9	31	46.0	45.0	
12	52.0	50.9	32	50.0	48.9	
13	50.0	48.9	33	35.0	34.2	
14	52.0	50.9	34	20.0	19.6	
15	48.0	46.9	35	9.0	8.8	
16	48.0	46.9	36	7.0	6.8	
17	54.0	52.8	37	6.0	5.9	
18	50.0	48.9	38	4.0	3.9	
19	50.0	48.9	39	4.0	3.9	
20	49.0	47.9	40	4.0	3.9	
averages:	48.6	47.6		32.2	31.5	

Drift Cal. Avg. VOC (ppm as propane) 39.5

Coors Brewing Company

#9 Can Filler Exhaust Vent

12-4-92

Method 25A : Measurement of Total Organic Concentration Using a Flame
Ionization Analyzer

Strip Chart Data

Hours 25 - 26

		Zero (%FS)	Span (%FS)	Actual Span (ppm)
Start	07:30	0.0	41.0	40.1
Stop	09:30	0.0	41.0	

point #	%FS VOC	ppm VOC	point #	%FS VOC	ppm VOC
1	4.0	3.9	21	36.0	35.2
2	20.0	19.6	22	35.0	34.2
3	36.0	35.2	23	34.0	33.3
4	42.0	41.1	24	32.0	31.3
5	42.0	41.1	25	31.0	30.3
6	39.0	38.1	26	34.0	33.3
7	39.0	38.1	27	34.0	33.3
8	37.0	36.2	28	36.0	35.2
9	26.0	25.4	29	32.0	31.3
10	42.0	41.1	30	39.0	38.1
11	31.0	30.3	31	38.0	37.2
12	42.0	41.1	32	40.0	39.1
13	42.0	41.1	33	38.0	37.2
14	37.0	36.2	34	34.0	33.3
15	42.0	41.1	35	41.0	40.1
16	42.0	41.1	36	41.0	40.1
17	43.0	42.1	37	42.0	41.1
18	35.0	34.2	38	42.0	41.1
19	40.0	39.1	39	42.0	41.1
20	38.0	37.2	40	42.0	41.1
averages:	36.0	35.2		37.1	36.3

Drift Cal. Avg. VOC (ppm as propane) 35.7

Coors Brewing Company
 #9 Can Filler Exhaust Vent
 12-4-92

Method 25A : Measurement of Total Organic Concentration Using a Flame
 Ionization Analyzer

Strip Chart Data

Hours 27 - 28

		Zero (%FS)	Span (%FS)	Actual Span (ppm)
Start	09:30	0.0	41.0	40.1
Stop	11:30	0.0	41.0	

point #	%FS VOC	ppm VOC	point #	%FS VOC	ppm VOC
1	35.0	34.2	21	39.0	38.1
2	31.0	30.3	22	41.0	40.1
3	41.0	40.1	23	31.0	30.3
4	41.0	40.1	24	36.0	35.2
5	42.0	41.1	25	39.0	38.1
6	43.0	42.1	26	40.0	39.1
7	41.0	40.1	27	37.0	36.2
8	39.0	38.1	28	38.0	37.2
9	28.0	27.4	29	40.0	39.1
10	30.0	29.3	30	calibrate	calibrate
11	42.0	41.1	31	calibrate	calibrate
12	40.0	39.1	32	37.0	36.2
13	calibrate	calibrate	33	39.0	38.1
14	calibrate	calibrate	34	37.0	36.2
15	calibrate	calibrate	35	39.0	38.1
16	calibrate	calibrate	36	41.0	40.1
17	36.5	35.7	37	calibrate	calibrate
18	39.0	38.1	38	calibrate	calibrate
19	39.0	38.1	39	36.0	35.2
20	40.0	39.1	40	11.0	10.8
averages:	38.0	37.1		36.3	35.5

Drift Cal. Avg. VOC (ppm as propane) 36.3

Coors Brewing Company

#9 Can Filler Exhaust Vent

12-4-92

Method 25A : Measurement of Total Organic Concentration Using a Flame

Ionization Analyzer

Strip Chart Data

Hours 29 - 30

		Zero (%FS)	Span (%FS)	Actual Span (ppm)
Start	11:30	0.0	41.0	40.1
Stop	13:30	0.5	39.0	

point #	%FS VOC	ppm VOC	point #	%FS VOC	ppm VOC
1	27.0	27.0	21	43.0	43.1
2	40.0	40.1	22	29.0	29.0
3	43.0	43.1	23	52.0	52.2
4	43.0	43.1	24	49.0	49.2
5	29.0	29.0	25	46.0	46.2
6	37.0	37.1	26	46.0	46.2
7	42.0	42.1	27	45.0	45.1
8	43.0	43.1	28	45.0	45.1
9	43.0	43.1	29	43.0	43.1
10	43.0	43.1	30	36.0	36.1
11	43.0	43.1	31	42.0	42.1
12	36.0	36.1	32	41.0	41.1
13	42.0	42.1	33	39.0	39.1
14	44.0	44.1	34	46.0	46.2
15	46.0	46.2	35	33.0	33.0
16	29.0	29.0	36	38.0	38.1
17	37.0	37.1	37	44.0	44.1
18	44.0	44.1	38	43.0	43.1
19	44.0	44.1	39	44.0	44.1
20	43.0	43.1	40	43.0	43.1
averages:	39.9	40.0		42.4	42.5

Drift Cal. Avg. VOC (ppm as propane) 41.2

Coors Brewing Company

#9 Can Filler Exhaust Vent

12-4-92

Method 25A : Measurement of Total Organic Concentration Using a Flame
Ionization Analyzer

Strip Chart Data

Hours 31 - 32

		Zero (%FS)	Span (%FS)	Actual Span (ppm)
Start	13:30	0.0	41.0	40.1
Stop	15:30	0.5	39.0	

point #	%FS VOC	ppm VOC	point #	%FS VOC	ppm VOC
1	44.0	44.1	21	43.0	43.1
2	45.0	45.1	22	44.0	44.1
3	22.0	21.9	23	40.0	40.1
4	40.0	40.1	24	37.0	37.1
5	43.0	43.1	25	31.0	31.0
6	43.0	43.1	26	20.0	19.9
7	43.0	43.1	27	33.0	33.0
8	42.0	42.1	28	27.0	27.0
9	44.0	44.1	29	37.0	37.1
10	27.0	27.0	30	32.0	32.0
11	42.0	42.1	31	25.0	25.0
12	41.0	41.1	32	28.0	28.0
13	36.0	36.1	33	27.0	27.0
14	36.0	36.1	34	46.0	46.2
15	19.0	18.9	35	45.0	45.1
16	37.5	37.6	36	45.0	45.1
17	41.0	41.1	37	45.0	45.1
18	45.0	45.1	38	44.0	44.1
19	42.0	42.1	39	45.0	45.1
20	44.0	44.1	40	44.0	44.1
averages:	38.8	38.9		36.9	37.0

Drift Cal. Avg. VOC (ppm as propane) 37.9

Coors Brewing Company

#9 Can Filler Exhaust Vent

12-4-92

Method 25A : Measurement of Total Organic Concentration Using a Flame
Ionization Analyzer

Strip Chart Data

Hours 33 - 34

		Zero (%FS)	Span (%FS)	Actual Span (ppm)
Start	15:30	0.0	40.0	40.1
Stop	17:30	0.0	40.0	

point #	%FS VOC	ppm VOC	point #	%FS VOC	ppm VOC
1	36.0	36.1	21	54.0	54.1
2	41.0	41.1	22	55.0	55.1
3	40.0	40.1	23	51.0	51.1
4	38.5	38.6	24	51.0	51.1
5	51.0	51.1	25	55.0	55.1
6	53.0	53.1	26	54.0	54.1
7	54.0	54.1	27	49.0	49.1
8	calibrate	calibrate	28	52.0	52.1
9	54.5	54.6	29	55.0	55.1
10	calibrate	calibrate	30	53.0	53.1
11	calibrate	calibrate	31	46.0	46.1
12	calibrate	calibrate	32	51.0	51.1
13	44.0	44.1	33	42.0	42.1
14	53.0	53.1	34	49.0	49.1
15	53.0	53.1	35	53.0	53.1
16	53.0	53.1	36	54.0	54.1
17	54.0	54.1	37	53.0	53.1
18	54.0	54.1	38	54.0	54.1
19	53.0	53.1	39	53.0	53.1
20	54.0	54.1	40	54.0	54.1
averages:	49.1	49.2		51.9	52.0

Drift Cal. Avg. VOC (ppm as propane) 50.6

Coors Brewing Company

#9 Can Filler Exhaust Vent

12-4-92

Method 25A : Measurement of Total Organic Concentration Using a Flame

Ionization Analyzer

Strip Chart Data

Hours 35 - 36

		Zero (%FS)	Span (%FS)	Actual Span (ppm)
Start	17:30	0.0	40.0	40.1
Stop	19:30	0.0	40.0	

point #	%FS VOC	ppm VOC	point #	%FS VOC	ppm VOC
1	54.0	54.1	21	30.0	30.1
2	55.0	55.1	22	50.0	50.1
3	54.0	54.1	23	27.0	27.1
4	54.0	54.1	24	30.0	30.1
5	49.0	49.1	25	43.0	43.1
6	50.0	50.1	26	44.0	44.1
7	51.0	51.1	27	42.0	42.1
8	55.0	55.1	28	31.0	31.1
9	55.0	55.1	29	45.0	45.1
10	54.0	54.1	30	52.0	52.1
11	44.0	44.1	31	48.0	48.1
12	20.0	20.1	32	51.0	51.1
13	14.0	14.0	33	51.0	51.1
14	11.0	11.0	34	47.0	47.1
15	9.0	9.0	35	24.0	24.1
16	8.0	8.0	36	43.0	43.1
17	6.5	6.5	37	39.0	39.1
18	6.0	6.0	38	44.0	44.1
19	5.5	5.5	39	20.0	20.1
20	5.0	5.0	40	10.0	10.0
averages:	33.0	33.1		38.5	38.6

Drift Cal. Avg. VOC (ppm as propane) 35.9

Coors Brewing Company
#9 Can Filler Exhaust Vent

12-4-92

Method 25A : Measurement of Total Organic Concentration Using a Flame
Ionization Analyzer

Strip Chart Data

Hours 37 - 38

		Zero (%FS)	Span (%FS)	Actual Span (ppm)
Start	19:30	0.0	40.0	40.1
Stop	21:30	0.0	40.0	

point #	%FS VOC	ppm VOC	point #	%FS VOC	ppm VOC
1	18.0	18.0	21	55.0	55.1
2	49.0	49.1	22	56.0	56.1
3	53.0	53.1	23	55.0	55.1
4	52.0	52.1	24	56.0	56.1
5	45.0	45.1	25	56.0	56.1
6	58.0	58.1	26	38.0	38.1
7	57.0	57.1	27	52.0	52.1
8	56.0	56.1	28	45.0	45.1
9	52.0	52.1	29	46.0	46.1
10	49.0	49.1	30	55.0	55.1
11	55.0	55.1	31	37.0	37.1
12	53.0	53.1	32	41.0	41.1
13	48.0	48.1	33	52.0	52.1
14	54.0	54.1	34	41.0	41.1
15	47.0	47.1	35	27.0	27.1
16	55.0	55.1	36	17.0	17.0
17	55.0	55.1	37	8.0	8.0
18	58.0	58.1	38	6.0	6.0
19	54.0	54.1	39	5.5	5.5
20	53.5	53.6	40	35.0	35.1
averages:	51.1	51.2		39.2	39.3

Drift Cal. Avg. VOC (ppm as propane) 45.2

Coors Brewing Company
 #9 Can Filler Exhaust Vent
 12-4-92

Method 25A : Measurement of Total Organic Concentration Using a Flame
 Ionization Analyzer

Strip Chart Data

Hours 39 - 40

		Zero (%FS)	Span (%FS)	Actual Span (ppm)
Start	21:30	0.0	40.0	40.1
Stop	23:30	0.0	40.0	

point #	%FS VOC	ppm VOC	point #	%FS VOC	ppm VOC
1	40.0	40.1	21	51.0	51.1
2	43.0	43.1	22	52.0	52.1
3	47.0	47.1	23	54.0	54.1
4	53.0	53.1	24	55.0	55.1
5	42.0	42.1	25	55.0	55.1
6	52.0	52.1	26	51.0	51.1
7	50.0	50.1	27	calibrate	calibrate
8	52.0	52.1	28	calibrate	calibrate
9	53.0	53.1	29	calibrate	calibrate
10	51.0	51.1	30	55.0	55.1
11	53.0	53.1	31	55.0	55.1
12	55.0	55.1	32	50.0	50.1
13	55.0	55.1	33	52.0	52.1
14	55.0	55.1	34	53.0	53.1
15	45.0	45.1	35	51.5	51.6
16	53.5	53.6	36	52.0	52.1
17	51.0	51.1	37	51.0	51.1
18	27.0	27.1	38	37.0	37.1
19	51.0	51.1	39	29.0	29.1
20	54.0	54.1	40	48.0	48.1
averages:	49.1	49.2		50.1	50.2

Drift Cal. Avg. VOC (ppm as propane) 49.7

Coors Brewing Company

#9 Can Filler Exhaust Vent

12-4/5-92

Method 25A : Measurement of Total Organic Concentration Using a Flame

Ionization Analyzer

Strip Chart Data

Hour 41

		Zero (%FS)	Span (%FS)	Actual Span (ppm)
Start	23:30	0.0	40.0	40.1
Stop	24:12	0.0	40.0	

point #	%FS VOC	ppm VOC
1	49.0	49.1
2	50.0	50.1
3	50.0	50.1
4	51.0	51.1
5	32.0	32.1
6	34.0	34.1
7	50.0	50.1
8	50.0	50.1
9	51.0	51.1
10	46.0	46.1
11	43.0	43.1
12	28.0	28.1
13	16.0	16.0
14	5.5	5.5
averages:	39.7	39.8

Drift Cal. Avg. VOC (ppm as propane) 39.8

Appendix 2
Sample Calculations

EPA Methods 1 - 4 : Determination of Volumetric Flow Rate and Molecular Weight

Sample Calculations

sample volume (dscf)

$$\begin{aligned} &= [17.64 (\text{°R/in Hg})] V_m Y [P_{\text{bar}} + (\Delta H/13.6)] / T_m \\ &= (17.64 \text{ °R/in Hg})(31.480 \text{ ft}^3)(1.0389)[24.604 + (3.0/13.6) \text{ inches Hg}] / (84 + 460 \text{ °R}) \\ &= 26.329 \text{ dscf} \end{aligned}$$

moisture volume (scf)

$$\begin{aligned} &= (0.04707 \text{ ft}^3/\text{ml}) V_{\text{ic}} \\ &= (0.04707 \text{ ft}^3/\text{ml})(7.5) \\ &= 0.353 \text{ scf} \end{aligned}$$

moisture content (%/100)

$$\begin{aligned} &= V_{w(\text{std})} / (V_{m(\text{std})} + V_{w(\text{std})}) \\ &= (0.353 \text{ scf}) / (26.329 \text{ dscf} + 0.353 \text{ scf}) \\ &= 0.0132 \end{aligned}$$

molecular weight dry (grams/mole)

$$\begin{aligned} &= 0.440(\% \text{CO}_2) + 0.320(\% \text{O}_2) + 0.280(\% \text{N}_2 + \% \text{CO}) \\ &= 0.440(0.0 \% \text{CO}_2) + (0.320)(20.9 \% \text{O}_2) + (0.280)(79.1 \% \text{N}_2) \\ &= 28.836 \text{ grams/mole} \end{aligned}$$

molecular weight actual (grams/mole)

$$\begin{aligned} &= M_a(1 - B_{ws}) + 18.0(B_{ws}) \\ &= (28.836 \text{ grams/mole})(1 - 0.0132) + (18.0)(0.0132) \\ &= 28.693 \text{ grams/mole} \end{aligned}$$

gas velocity (ft/sec)

$$\begin{aligned} &= \{85.49 \text{ ft/sec} [(\text{lb/lb-mole})(\text{in. Hg}) / (\text{°R})(\text{in. H}_2\text{O})]^{1/2}\} C_p (\Delta p^{1/2})_{\text{avg}} (T_{s(\text{avg})} / P_s M_s)^{1/2} \\ &= (85.49)(0.84)(0.1885) \{ (72 + 460) / [(24.604 + 0.07/13.6)(28.693)] \}^{1/2} \\ &= 11.7 \text{ ft/sec} \end{aligned}$$

gas flow (acfm)

$$\begin{aligned} &= A_{vs}(60 \text{ seconds/minute}) \\ &= (\pi)(22.0/12 \text{ ft})^2 (11.7 \text{ ft/sec})(60)/4 \\ &= 1861 \text{ acfm} \end{aligned}$$

gas flow (dscfm)

$$\begin{aligned} &= (60 \text{ seconds/minute})(1 - B_{ws}) V_s A T_{\text{std}} P_s / (T_{s(\text{avg})} P_{\text{std}}) \\ &= (60)(1 - 0.0353)(11.7)(\pi)(22.0/12 \text{ ft})^2 (528)(24.604 + 0.07/13.6) / [(72 + 460)(29.92)(4)] \\ &= 1499 \text{ dscfm} \end{aligned}$$

EPA Methods 1 - 4 : Determination of Volumetric Flow Rate and Molecular Weight

Variables

A = Stack cross-sectional area (ft²)

B_{ws} = Water vapor in the gas stream, proportion by volume

C_p = Pitot coefficient (0.84 dimensionless)

ΔH = Average pressure differential across the orifice meter (in. H₂O)

Δp = Velocity head of stack gas (in. H₂O)

M_d = Molecular weight of dry stack gas (lb/lb mole)

M_s = Molecular weight of wet stack gas (lb/lb mole)

P_{bar} = Barometric pressure (in. Hg)

P_g = Sack pressure relative to ambient (in. H₂O)

P_s = Absolute stack pressure (in. Hg)

P_{std} = Standard atmospheric pressure (29.92 in. Hg)

Q_a = Actual volumetric air flow out of stack (acfm)

Q_{std} = Volumetric air flow out of stack corrected to standard conditions (dscfm)

T_m = Average meter temperature (°F + 460 = °R)

T_{s(avg)} = Average stack temperature (°F + 460 = °R)

T_{std} = Standard temperature (528 °R)

V_{lc} = volume of moisture collected from gas sample (ml)

v_s = Stack gas velocity (ft/sec)

V_m = Volume of gas through dry gas meter (ft³)

V_{m(std)} = Volume of gas through dry gas meter corrected to standard conditions (dscf)

V_{w(std)} = Volume of water vapor in gas sample at standard conditions (scf)

Y = Dry gas meter calibration factor (dimensionless)

Q = Total sampling time (minutes)

EPA Method 25A : Measurement of Total Organic Concentration Using a Flame Ionization Analyzer

Sample Calculations

drift cal. ppm as propane

$$= \frac{[(\%FS \text{ analyzer stack value}) - (\%FS \text{ analyzer average 0 value})](\text{span gas value ppm})}{[(\%FS \text{ analyzer average span value}) - (\%FS \text{ analyzer average 0 value})]}$$

$$= \frac{(28.0 \%FS) - [(0.0 \%FS + 0.5 \%FS) / 2](40.1 \text{ ppm})}{[(39.5 \%FS + 39.0 \%FS) / 2] - [(0.0 \%FS + 0.5 \%FS) / 2]}$$

$$= 28.6 \text{ ppm VOC as propane}$$

VOC emissions, Theoretical Total (lb/hr as propane)

$$= \frac{[\text{avg. VOC conc. (ppm)}][\text{stack flow (dscfm)}](60 \text{ min/hr})(28.317 \text{ liter/ft}^3)(44.09 \text{ g/mole})(2.205 \text{ lb/kg})}{(24.055 \text{ liters/mole @ STP})(1000 \text{ g/kg})(1 \times 10^6)(1 - \%H_2O/100)}$$

$$= \frac{(28.6 \text{ ppm})(1874 + 1871 + 1829 \text{ dscfm})(60)(28.317)(44.09)(2.205)}{(24.055)(1000)(1 \times 10^6)(1 - 0.013)}$$

$$= 1.11 \text{ lb/hr VOC}$$

VOC emissions, Theoretical from Filling (lb/hr as propane)

$$= \frac{[(\text{VOC outlet (ppm)})(\Sigma \text{flow (dscfm)}) - \Sigma[(\text{VOC ppm})(\text{flow dscfm}) \text{ inlet}]](60)(28.317)(44.09)(2.205)}{(24.055 \text{ liters/mole @ STP})(1000 \text{ g/kg})(1 \times 10^6)(1 - \%H_2O/100)}$$

$$= \frac{[(28.6 \text{ ppm})(5574 \text{ dscfm}) - (2.0)(1874) - (2.5)(1871) - (3.0)(1829)](60)(28.317)(44.09)(2.205)}{(24.055)(1000)(1 \times 10^6)(1 - 0.013)}$$

$$= 1.01 \text{ lb/hr as propane}$$

VOC emissions (lb/hr as ethanol)

$$= [\text{VOC emissions (lb/hr as propane)}](2.506 \text{ empirical conversion factor})$$

$$= 2.78 \text{ lb/hr as ethanol}$$

VOC emissions (lb/bbl as ethanol)

$$= [\text{VOC emissions (lb/hr as ethanol)}]/[\text{beer filling rate (bbl/hr)}]$$

$$= (2.78)/(85.3)$$

$$= 0.0326 \text{ lb/bbl as ethanol}$$

Ethanol / Propane Conversion

Sample Calculations

ethanol (mg/dscm)

$$= \frac{[\text{mass ethanol (g)}][\text{temp (}^{\circ}\text{F)} + 460][1013 \text{ (std. press. mbar)}][1000 \text{ (ltrs/m}^3\text{)}][1000 \text{ (mg/g)}]}{[\text{sampling time (min)}][\text{sampling rate (lpm)}][528 \text{ (std. temp. R)}][P_b \text{ (mbar)}]}$$

$$= \frac{(0.0204)(70 + 460)(1013)(1000)(1000)}{(15.0)(1.85)(528)(842)}$$

$$= 890 \text{ mg/dscm ethanol}$$

propane (mg/dscm)

$$= [\text{propane conc. (ppm)}][44.09 \text{ (mg/mmol propane)}]/[24.055 \text{ (ml/mmol @ STP)}]$$

$$= (201.4)(44.09)/(24.055)$$

$$= 369 \text{ mg dscm propane}$$

conversion factor

$$= [\text{ethanol (mg/dscm)}]/[\text{propane (mg/dscm)}]$$

$$= (890)/(369)$$

$$= 2.411 \text{ mass/volume conversion factor}$$

carbon-basis conversion factor

$$= \frac{(\text{carbon mass fraction, propane})}{(\text{carbon mass fraction, ethanol})(\text{empirical mass/vol conversion factor})}$$

$$= (36/44.09)/[(24/46.07)(2.506)]$$

$$= 0.625$$

published carbon-basis conversion factor

$$= 0.66$$

carbon-basis conversion factor % difference

$$= \frac{[(\text{experimental conversion factor}) - (\text{published conversion factor})](100)}{(\text{published conversion factor})}$$

$$= \frac{[(0.625) - (0.66)](100)}{(0.66)}$$

$$= -5.3\% \text{ difference}$$

Appendix 3
Field Data

**#3 Bottle Filler
Methods 1 - 4
Field Data Sheets**

CO ₂ (%)	0.0
Assumed Moisture (%)	1
Ambient Temperature (oF)	75
Probe Length (ft)	2
Probe Temperature (oF)	/
Nozzle Diameter (in)	/
Sonic Pressure (in H ₂ O)	+ 0.08
Filter ID#	/
CO ₂ (%)	20.9
Barometric Pressure (mbar)	838
Probe Material	PTFE
Filter Temperature (oF)	/
Moisture (grams)	7.0
Start Time	10:55
Stop Time	
Method	1-4

PC: CB, 30105

[illegible]

CO ₂ (%)	20	0.0	—	Assumed Moisture (%)	—	CO ₂ (%)	20.9
Probe Length (ft)	2	—	—	Ambient Temperature (oF)	75	Barometric Pressure (mbar)	833
Probe Temperature (oF)	—	—	—	Probe Material	PTFE	Filler Temperature (oF)	—
Probe Temperature (in)	—	—	—	Moisture (grams)	4.0	Start Time	12:30
Nozzle Diameter (in)	—	—	—	Static Pressure (in H ₂ O)	40.07	Stop Time	—
Filter ID#	—	—	—	Method	1- 24		

Air Pollution Testing, Inc.
Schematic of Stack Cross Section

24.5

18.5"

1 2 3

$A = 3.15$

CO ₂ (%)	0.0	0	20.9	20.9
Assumed Moisture (%)				
Ambient Temperature (oF)	70	SS		
Probe Length (in)	4			
Probe Temperature (oF)				
Moisture (grams)				
Nozzle Diameter (in)				
Static Pressure (in H ₂ O)	+3.8			
Start Time				
Stop Time				
Filter ID#				Method 1-2

PC: CB30105

[illegible]

[illegible]

Air Pollution Testing, Inc.
Schematic of Slack Cross Section

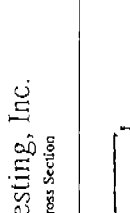
14.5"

10.5"

A=1.06

PC:B30105

[illegible]



A schematic diagram of a rectangular stack cross-section. The diagram is a rectangle with a horizontal width of 10.5" and a vertical height of 14.5". The dimensions are labeled with handwritten text: "10.5\"" at the top and "14.5\"" on the right side.

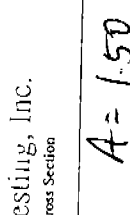
CO ₂ (%)	0.0	02 (%)	20.9
Assumed Moisture (%)	0	Baometric Pressure (mbar)	833
Ambient Temperature (oF)	70	Probe Material	SS
Probe Length (ft)	4	Filler Temperature (oF)	—
Probe Temperature (oF)	—	Moisture (grams)	—
Nozzle Diameter (in)	—	Start Time	—
Static Pressure (in H ₂ O)	+1.4	Stop Time	—
Filter ID#	—	Method	1-2

[illegible]

Air Pollution Testing, Inc.
Schematic of Stack Cross Section

$12" \times 18"$

$A = 1.50$

A hand-drawn schematic of a rectangular stack cross-section. The rectangle is oriented horizontally. To the left of the rectangle, the dimensions "12" x 18" are written vertically. Above the rectangle, the area "A = 1.50" is written. The rectangle itself is drawn with simple lines, and there are small tick marks on the top and right edges.[illegible]

Air Pollution Testing, Inc.
Schematic of Stack Cross Section

18"

12"

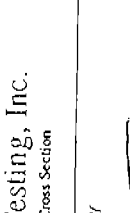
1 2 3

4-1.50

CO2 (%)	0.0	O2 (%)	20.9
Assumed Moisture (%)	0	Barometric Pressure (inbar)	833
Ambient Temperature (oF)	70	Probe Material	SS
Probe Length (ft)	4	Filler Temperature (oF)	/
Probe Temperature (oF)	/	Moisture (grams)	/
Nozzle Diameter (in)	/	Start Time	/
Static Pressure (in H2O)	+1.0	Stop Time	/
Filter ID#	/	Method	1-2

[illegible]

Air Pollution Testing, Inc.
Schematic of Stack Cross Section



18.0"

12.0"

CO ₂ (%)	0.0	O ₂ (%)	20.9
Assumed Moisture (%)	0	Barometric Pressure (mbar)	82.9
Ambient Temperature (oF)	70	Probe Material	SS
Probe Length (ft)	/	Filler Temperature (oF)	/
Probe Temperature (oF)	/	Moisture (grams)	/
Nozzle Diameter (in)	/	Start Time	/
Sonic Pressure (in H ₂ O)	+ 1.1	Stop Time	/
Filler ID#	/	Method	1-2

[illegible]

**#5 Can Filler
Methods 1 - 4
Field Data Sheets**

Plant	Coors	Date	12-2-72
Location	5 Can Outlet		
Operator	PO/AM		
Run Number	1	Pilot Tube Coefficient	0.84
Sample Box ID#		Master Box ID#	
Meter ΔH	1.683	C Factor	
Pre-Test Pilot Leak Check	☒	Post-Test Pilot Leak Check	☒
Pre-Test Pump Leak Check	☒	Post-Test Pump Leak Check	☒

PC: CB 30105

00 12/4/72 00 15/4/72

Air Pollution Testing, Inc. Schematic of Stack Cross Section	

CO ₂ (%)	0.0	O ₂ (%)	20.9
Assured Moisture (%)	75	Barometric Pressure (mbar)	828
Ambient Temperature (oF)	75	Probe Material	NFE
Probe Length (ft)	3	Filter Temperature (oF)	
Probe Temperature (oF)		Moisture (grams)	9.0
Nozzle Diameter (in)		Start Time	17:02
Static Pressure (in H ₂ O)	-2.6	Stop Time	17:52
Filter ID#		Method	1-4

Traverse Point	Sampling Time (minutes)	Vacuum (in Hg)	Velocity Head (in H ₂ O)	Pressure Differential (in H ₂ O)	Gas Volume (ft ³) Initial Volume	Stack Temp. (oF)	Probe Temp. (oF)	Pilot Temp. (oF)	Gas Temp. Inlet (oF) Outlet (oF)	Condenser Temp. (oF)	Notes
1-1	10	7	0.32	3.5	380.10	70			77 77	62	VUC = -1.0ml + 10.0g
2	20	7	0.41	3.5	391.31	70			80 78	58	
3	30	7	0.34	3.5	402.61	69			83 79	54	
4	40	7	0.29	3.5	413.75	69			90 81	55	
45	50	7	0.50	3.5	425.09	68			94 83	57	
6			0.93			67					
7			1.14			67					
8			1.29			67					
2-1			1.10			69					
2			0.91			69					
3			0.85			68					
4			0.60			67					
5			0.75			67					
6			0.83			66					
7			0.92			66					
8			0.86			66					
					56.039	66					
					56.039	66					

✓ 0.8462

68

72

Plant	Corgs	Date	12-2-92
Location	5 can outlet		
Operator	RO/MM		
Run Number	2	Pilot Tube Coefficient	0.84
Sample Box ID#		Meter Box ID#	
Meter ΔH ₀	1.683	C Factor	
Pre-Test Pilot Leak Check	✓	Post-Test Pilot Leak Check	✓
Pre-Test Pump Leak Check	0 @ 10" Hg	Post-Test Pump Leak Check	0 @ 10" Hg

PC: 6330105

Air Pollution Testing, Inc.
Schematic of Stack Cross Section

CO ₂ (%)	0.0	O ₂ (%)	20.9
Assured Moisture (%)		Barometric Pressure (inbar)	Q28
Ambient Temperature (oF)	75	Probe Material	P7FE
Probe Length (ft)	3	Filler Temperature (oF)	
Probe Temperature (oF)		Moisture (grams)	5.0
Nozzle Diameter (in)		Start Time	18:15
Static Pressure (in H ₂ O)	-2.8	Stop Time	
Filter ID#		Method	1-4

Traverse Point	Sampling Time (minutes)	Vacuum (in Hg)	Velocity Head (in H ₂ O)	Pressure Differential (in H ₂ O)	Gas Volume (ft ³) Initial Volume	Stack Temp. (oF)	Probe Temp. (oF)	Filter Temp. (oF)	Gas Temp. Inlet (oF) Outlet (oF)	Condenser Temp. (oF)	Notes
1-1	10		0.31	3.5	425.111	71			84 81		V _{LC} = 5.0g + 0.0 ncl
2	20		0.35	3.5	445.61	71			94 84		4cm ~ 3877
3	30		0.33	3.5	455.929	71			96 86		4cm ~ 3105
4			0.28			70					
5			0.53			69					
6			0.91			67					
7			1.10			67					
8			1.25			66					
2-1			1.15			69					
2			0.93			69					
3			0.83			68					
4			0.59			67					
5			0.73			66					
6			0.87			66					
7			0.91			66					
8			0.86			66					
					30.818						

1.8478 ✓

68 ✓

68 ✓

Plant	cor5	Date	12-2-92
Location	5 can outlot		
Operator	100 / am		
Run Number	3	Pilot Tube Coefficient	.84
Sample Box ID#		Meter Box ID#	
Meter ΔH@	1.683	C Factor	
Pre-Test Pilot Leak Check	✓	Post-Test Pilot Leak Check	✓
Pre-Test Pump Leak Check	0@18" Hg	Post-Test Pump Leak Check	0@17" Hg

PC: CB30105

Air Pollution Testing, Inc.
Schematic of Stack Cross Section

CO2 (%)	0.0	O2 (%)	20.9
Assumed Moisture (%)		Barometric Pressure (mbar)	82.7
Ambient Temperature (oF)	78	Probe Material	PTE
Probe Length (ft)	3	Filler Temperature (oF)	
Probe Temperature (oF)		Moisture (grams)	
Nozzle Diameter (in)		Start Time	19:20
Static Pressure (in H2O)	-2.4	Stop Time	19:50
Filter ID#		Method	1-4

Traverse Point	Sampling Time (minutes)	Vacuum (in Hg)	Velocity Head (in H2O)	Pressure Differential (in H2O)	Gas Volume (ft ³) Initial Volume	Stack Temp. (oF)	Probe Temp. (oF)	Pilot Temp. (oF)	Inlet Gas Temp. (oF)	Outlet Gas Temp. (oF)	Condenser Temp. (oF)	Notes
1-1	10	7	0.44	3.5	456.115	71			83	83	69	V _{LC} = 6.0 g + 0.0 ml
2	20	7	0.32	3.6	477.96	70			84	84	62	
3	30	7	0.40	3.6	489.444	70			85	88	65	
4			0.37			70						
5			0.34			69						
6			0.56			67						
7			1.10			67						
8			1.30			67						
2-9			0.87			69						
2			0.71			68						
3			0.71			67						
4			0.63			66						
5			0.71			66						
6			0.87			65						
7			0.86			65						
8			0.86			65						

✓ 18(45)

✓ (12)

88

Air Pollution Testing, Inc.
Schematic of Stack Cross Section

1
2
3

26"

27.8'

$25\frac{7}{8}'' \times 15\frac{7}{8}'' = 10$

$A = 2.853 \text{ sf}$

PC: CB30105

[illegible]

CO ₂ (%)	0.0	O ₂ (%)	20.9
Assumed Moisture (%)	0	Barometric Pressure (mbar)	838
Ambient Temperature (oF)	70	Probe Material	SS
Probe Length (ft)	2	Filter Temperature (oF)	—
Probe Temperature (oF)	—	Moisture (grams)	—
Nozzle Diameter (in)	—	Start Time	—
Static Pressure (in H ₂ O)	+1.3	Stop Time	—
Filter ID#	—	Method	1-2

[illegible]

CO ₂ (%)	0.0	20.9	
Assumed Moisture (%)	0		838
Ambient Temperature (oF)	70	SS	
Probe Length (ft)	2		
Probe Temperature (oF)			
Nozzle Diameter (in)			
Static Pressure (in H ₂ O)	+1.3		
Filler ID#			1-2

[illegible]

CO ₂ (%)	0.0	CO ₂ (%)	20.9
Assumed Moisture (%)	0	Barometric Pressure (mbar)	837
Ambient Temperature (oF)	70	Probe Material	SS
Probe Length (ft)	2	Filter Temperature (oF)	
Probe Temperature (oF)		Moisture (grams)	
Nozzle Diameter (in)		Start Time	
Static Pressure (in H ₂ O)	4.29	Stop Time	
Filter ID#		Method	

Assumed Moisture (%)	0	Baometric Pressure (mbar)	938
Ambient Temperature (oF)	70	Probe Material	SS
Probe Length (ft)	Z	Filter Temperature (oF)	/
Probe Temperature (oF)	/	Moisture (grams)	/
Nozzle Diameter (in)	/	Start Time	/
Static Pressure (in H2O)	34	Stop Time	/
Filter ID#		Method	1-7

PC: CB 30105

[illegible]

**#6 Can Filler
Methods 1 - 4
Field Data Sheets**

Air Pollution Testing, Inc.
Schematic of Stack Cross Section

24" x 10"

○

ID = 17.5'

CO ₂ (%)	0
Assured Moisture (%)	✓
Ambient Temperature (oF)	75
Probe Length (ft)	2
Probe Temperature (oF)	✓
Nozzle Diameter (in)	✓
Static Pressure (in H ₂ O)	-0.48
Filler ID#	
Barometric Pressure (mbars)	834
Probe Material	PTFE
Filler Temperature (oF)	✓
Moisture (grams)	4.5
Start Time	11:30
Stop Time	12:00
Method	1-4

Traverse Point	Sampling Time (minutes)	Vacuum (in Hg)	Velocity Head (in H ₂ O)	Pressure Differential (in H ₂ O)	Gas Volume (ft ³) Initial Volume	Stack Temp. (°F)	Probe Temp. (°F)	Pitot Temp. (°F)	Inlet (°F) Gas Temp.	Outlet (°F)	Condenser Temp. (°F)	Notes
1-1	10	5	.15	3.0	165.555 175.30	75			91	82	60	Vic = 4.5 g + 0 ml
2	20	5	.14	3.0	185.11	74			95	87	51	
3	30	5	.13	3.0	196.703	74			101	89	50	
4			.14			73						
5			.19			72						
6			.17			72						
7			.16			73						
8			.17			72						
2-1			.18			65						
2			.13			66						
3			.14			64						
4			.15			63						
5			.13			63						
6			.11			63						
7			.13	3.0	31.148	62						
8			.11	3.0	63	63						

Total 3805 V
 68

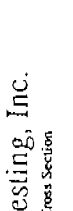
A hand-drawn schematic of a stack cross-section. It is a rectangle with a width of 18.0 inches and a height of 26.0 inches. The right side of the rectangle has five vertical tick marks, and the top edge has a small horizontal tick mark on the right side.

Assumed Moisture (%)	0.0	Assumed Moisture (%)	0.2 (56)
Probe Length (ft)	4	Probe Length (ft)	20.9
Probe Temperature (oF)	75	Probe Temperature (oF)	836
Probe Temperature (oF)		Probe Temperature (oF)	
Moisture (grams)		Moisture (grams)	
Nozzle Diameter (in)		Nozzle Diameter (in)	
Static Pressure (in H2O)	4.28	Static Pressure (in H2O)	10.30
Filter ID#		Filter ID#	
Method	1-2	Method	

PC: CB30105

[illegible]

Air Pollution Testing, Inc.
Schematic of Stack Cross Section

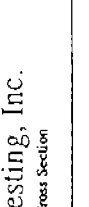


26" x 18"

PC: CB 30105

[illegible]

Air Pollution Testing, Inc.
Schematic of Slack Cross Section

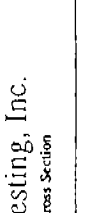


26" x 18"

CO ₂ (%)	0.0	0.0	20.9
Assumed Moisture (%)	0.0		Barometric Pressure (mbar) 836
Ambient Temperature (oF)	75		Probe Material SS
Probe Length (in)	4		Filler Temperature (oF)
Probe Temperature (oF)			Moisture (grams)
Nozzle Diameter (in)			Start Time 13:30
Static Pressure (in H ₂ O)	+2.7		Stop Time
Filler ID#			Method 1-2

[illegible]

Air Pollution Testing, Inc.
Schematic of Stack Cross Section

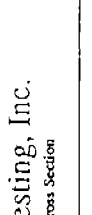


15" x 15"

CO ₂ (%)	0.0	O ₂ (%)	20.9
Assumed Moisture (%)	0.0	Barometric Pressure (inbar)	836
Ambient Temperature (oF)	75	Probe Material	SS
Probe Length (ft)	4	Filter Temperature (oF)	/
Probe Temperature (oF)	/	Moisture (grams)	/
Nozzle Diameter (in)	/	Start Time	/
Static Pressure (in H ₂ O)	+1.94	Stop Time	/
Filter ID#	/	Method	1-2

[illegible]

Air Pollution Testing, Inc.
Schematic of Stack Cross Section

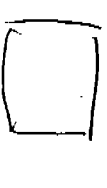


15" x 15"

CO ₂ (%)	0.0	0.2	0.9
Assumed Moisture (%)	0.0	0.0	0.0
Ambient Temperature (oF)	75	75	75
Probe Length (in)	4	4	4
Probe Temperature (oF)			
Moisture (grams)			
Nozzle Diameter (in)			
Static Pressure (in H ₂ O)			
Filter ID#			

[illegible]

Air Pollution Testing, Inc.
Schematic of Stack Cross Section



15" x 15"

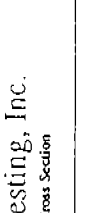
PG: CB30105

[illegible]

**#9 Can Filler
Methods 1 - 4
Field Data Sheets**

Air Pollution Testing, Inc.

Schematic of Stack Cross Section



$11 \frac{7}{8}'' \times 13 \frac{7}{8}''$

CO ₂ (%)	0.0	O ₂ (%)	20.9
Assumed Moisture (%)	0	Barometric Pressure (mbar)	828
Ambient Temperature (°F)	75	Probe Material	SS
Probe Length (ft)	4	Filter Temperature (°F)	—
Probe Temperature (°F)	—	Moisture (grams)	—
Nozzle Diameter (in)	—	Start Time	—
Static Pressure (in H ₂ O)	-0.41	Stop Time	—
Filter ID#	—	Method	1-2

[illegible]

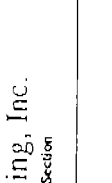
Air Pollution Testing, Inc.
Schematic of Stack Cross Section

A hand-drawn schematic of a rectangular stack cross-section. The rectangle is oriented vertically. To the left of the rectangle, the dimension "13 7/8" is written vertically. To the right of the rectangle, the dimension "11 7/8" is written vertically. The rectangle is drawn with simple black lines on a white background.

CO2 (%)	0.0	20.9	O2 (%)
Assumed Moisture (%)	0	82.7	Barometric Pressure (mbar)
Ambient Temperature (oF)	75	55	Probe Material
Probe Length (in)	4	—	Filter Temperature (oF)
Probe Temperature (oF)	—	—	Moisture (grams)
Nozzle Diameter (in)	—	—	Start Time
Static Pressure (in H2O)	-0.40	—	Stop Time
Filter ID#	—	—	Method
			1-2

[illegible]

Air Pollution Testing, Inc.
Schematic of Slack Cross Section



A hand-drawn schematic of a rectangular cross-section. The rectangle is oriented vertically. To the right of the rectangle, the dimensions are written as $13\frac{7}{8}$ inches (width) and $11\frac{7}{8}$ inches (height).

CO ₂ (%)	0.0	0.2	20.7
Assumed Moisture (%)	0		82.9
Ambient Temperature (oF)	75		SS
Probe Length (ft)	4		Probe Material
Probe Temperature (oF)	/		Filler Temperature (oF)
Probe Temperature (oF)	/		Moisture (grams)
Nozzle Diameter (in)	/		Start Time
Static Pressure (in H ₂ O)	-0.29		Stop Time
Filter ID#	/		Method
			1-2

[illegible]

Air Pollution Testing, Inc.
 Schematic of Stack Cross Section

CO ₂ (%)	0.0	0	20.9	
Assumed Moisture (%)		0		Barometric Pressure (inbar)
		75		528
Ambient Temperature (oF)			55	Probe Material
Probe Length (ft)	4			Filler Temperature (oF)
Probe Temperature (oF)				Moisture (grams)
Nozzle Diameter (in)				Start Time
Static Pressure (in H ₂ O)		-0.40		Stop Time
Filter ID#				Method
				12

[illegible]

CO ₂ (%)	0.0	0.2	0.2
Assumed Moisture (%)	0	75	82.7
Ambient Temperature (oF)	4	55	55
Probe Length (in)	4	55	55
Probe Temperature (oF)	4	55	55
Nozzle Diameter (in)	4	55	55
Static Pressure (in H ₂ O)	4	55	55
Filter ID#	4	55	55

Air Pollution Testing, Inc.
Schematic of Stack Cross Section

15 $\frac{3}{4}$ "

23 $\frac{7}{8}$ "

CO2 (%)	0.0	O2 (%)	20.9
Assumed Moisture (%)	0	Barometric Pressure (inbar)	828
Ambient Temperature (oF)	75	Probe Material	SS
Probe Length (ft)	4	Filler Temperature (oF)	/
Probe Temperature (oF)	/	Moisture (grams)	/
Nozzle Diameter (in)	/	Start Time	/
Static Pressure (in H2O)	41.90	Stop Time	/
Filter ID#	/	Method	1-2

[illegible]

Air Pollution Testing, Inc.
Schematic of Stack Cross Section

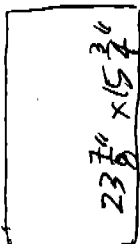


23 7/16 x 15 9/16

CO2 (%)	0.0					
Assumed Moisture (%)	0					
Ambient Temperature (oF)	75					
Probe Length (ft)	4					
Probe Temperature (oF)						
Moisture (grams)						
Nozzle Diameter (in)						
Static Pressure (in H2O)	+1.40					
Stop Time						
Start Time						
Filter ID#						
Method						
Probe Material	5S					
Barometric Pressure (mbar)	829					
O2 (%)	20.9					

[illegible]

Air Pollution Testing, Inc.
Schematic of Stack Cross Section



23 $\frac{7}{8}$ x 15 $\frac{3}{4}$

CO ₂ (%)	0.0	O ₂ (%)	20.9
Assumed Moisture (%)	0	Barometric Pressure (mbar)	828
Ambient Temperature (oF)	75	Probe Material	SS
Probe Length (ft)	4	Filter Temperature (oF)	/
Probe Temperature (oF)	/	Moisture (grams)	/
Nozzle Diameter (in)	/	Start Time	/
Sonic Pressure (in H ₂ O)	+1.40	Stop Time	/
Filter ID#	/	Method	1-2

[illegible]

Air Pollution Testing, Inc.
Schematic of Stack Cross Section

[illegible]

Plant	Coors Brewing	Date	12-3-92
Location	#9 Can Filler Vent		
Operator	PO/MM		
Run Number	2	Pilot Tube Coefficient	0.84
Sample Box ID#		Meter Box ID#	
Meter ΔH@	1.683	C Factor	
Pre-Test Pilot Leak Check	✓	Post-Test Pilot Leak Check	✓
Pre-Test Pump Leak Check	001144	Post-Test Pump Leak Check	001044

Y4=10389

PCICB 30105

Air Pollution Testing, Inc.	
Schematic of Stack Cross Section	
10 = 15.5"	

CO ₂ (%)	0.0	O ₂ (%)	20.9
Assumed Moisture (%)		Barometric Pressure (inbar)	827
Ambient Temperature (oF)	75	Probe Material	
Probe Length (ft)		Filter Temperature (oF)	
Probe Temperature (oF)		Moisture (grams)	3.0
Nozzle Diameter (in)		Start Time	
Static Pressure (in H ₂ O)	-3.0	Stop Time	
Filter ID#		Method	1-4

Traverse Point	Sampling Time (minutes)	Vacuum (in Hg)	Velocity Head (in H ₂ O)	Pressure Differential (in H ₂ O)	Gas Volume (cu) Initial Volume	Stack Temp. (oF)	Probe Temp. (oF)	Filter Temp. (oF)	Gas Temp. Inlet (oF) Outlet (oF)	Condenser Temp. (oF)	Notes
1-1	10	7	.55	3.5	538.510	72			81 80	67	
2	20	7	.62	3.5	548.65	72			85 81	48	
3	30	7	.46	3.5	559.11	71			93 82	49	
4			.34		570.031	71					
5			.23			71					
6			.19			70					
7			.28			70					
8			.31			70					
2-1			.29			70					
2			.31			70					
3			.25			69					
4			.22			69					
5			.38			69					
6			.41			69					
7			.48			68					
8			.60			68					

(15988)

(70)

31.521

35

84

Plant	Coors Brewing	Date	12-4-92
Location	#9 Can Filter Vent		
Operator	PO/MM		
Run Number	4	Pilot Tube Coefficient	.84
Sample Box ID#		Merit Box ID#	
Meter ΔH ₀	1.683	C Factor	
Pre-Test Pilot Leak Check	✓	Post-Test Pilot Leak Check	✓
Pre-Test Pump Leak Check	0012144	Post-Test Pump Leak Check	0012144

Yd = 1.0389

PC: CB30105

Air Pollution Testing, Inc.	
Schematic of Stack Cross Section	

CO ₂ (%)	0.0	O ₂ (%)	20.9
Assumed Moisture (%)	✓	Barometric Pressure (inbar)	828
Ambient Temperature (oF)		Probe Material	
Probe Length (ft)		Filter Temperature (oF)	✓
Probe Temperature (oF)		Moisture (grams)	2.5
Nozzle Diameter (in)		Start Time	
Static Pressure (in H ₂ O)	-3.0	Stop Time	
Filter ID#		Method	1-4

Traverse Point	Sampling Time (minutes)	Vacuum (in Hg)	Velocity Head (in H ₂ O)	Pressure Differential (in H ₂ O)	Gas Volume (ft ³) Initial Volume	Stack Temp. (oF)	Probe Temp. (oF)	Filter Temp. (oF)	Inlet (oF) Gas Temp. Outlet (oF)	Condenser Temp. (oF)	Notes
1-1	10	7	.63	3.5	603.111	71			77 77	58	
2	20	7	.55	3.5	624.81	71			87 79	52	
3	30	7	.47	3.5	635.222	71			96 82	52	
4			.36			71					
5			.22			71					
6			.22			71					
7			.29			71					
8			.28			71					
2-1			.30			71					
2			.31			71					
3			.17			70					
4			.29			70					
5			.40			70					
6			.48			70					
7			.44			70					
8			.51			70					

(5990) (71) (71)

Plant	Coors Brewing	Date	12-4-92
Location	#9 Can Filler Vent		
Operator	PO/M/M		
Run Number	5	Pilot Tube Coefficient	.84
Sample Box ID#		Meter Box ID#	
Meter ΔH ₀	1.683	C Factor	
Pre-Test Pilot Leak Check	V	Post-Test Pilot Leak Check	V
Pre-Test Pump Leak Check	00.1144	Post-Test Pump Leak Check	00.1044

Yd = 1.8289 PC: CB 30165

Air Pollution Testing, Inc.	
Schematic of Stack Cross Section	
ID = 15.5"	

CO ₂ (%)	0.0	O ₂ (%)	20.9
Assumed Moisture (%)		Barometric Pressure (mbar)	827
Ambient Temperature (oF)	75	Probe Material	
Probe Length (ft)		Filter Temperature (oF)	
Probe Temperature (oF)		Moisture (grams)	4.0
Nozzle Diameter (in)		Start Time	
Static Pressure (in H ₂ O)	-30	Stop Time	
Filter ID#		Method	1-4

Traverse Point	Sampling Time (minutes)	Vacuum (in Hg)	Velocity Head (in H ₂ O)	Pressure Differential (in H ₂ O)	Gas Volume (ft ³) Initial Volume	Suck Temp. (oF)	Probe Temp. (oF)	Pilot Temp. (oF)	Gas Temp. Inlet (oF) Outlet (oF)	Condenser Temp. (oF)	Notes
1-1	10	7	.60	3.5	635.826	71			79 80	66	
2	20	7	.58	3.5	656.91	70			86 80	60	
3	30	7	.51	3.5	667.504	70			97 82	65	
4			.32			70					
5			.25			71					
6			.25			71					
7			.31			71					
8			.44			71					
29			.30			71					
2			.29			71					
3			.15			70					
4			.27			71					
5			.36			71					
6			.45			71					
7			.44			71					
8			.50			71					

54
 31.678
 35
 1.6030
 79

Air Pollution Testing, Inc.
Schematic of Stack Cross Section

14"
12"
11 7/8"
13 7/8"

CO ₂ (%)	0.0	0.0	20.9
Assumed Moisture (%)	0		Barometric Pressure (mbar)
Ambient Temperature (oF)	70		Probe Material
Probe Length (ft)	2		Filter Temperature (oF)
Probe Temperature (oF)			Moisture (grams)
Nozzle Diameter (in)			Start Time
Static Pressure (in H ₂ O)	-0.44		Stop Time
Filter ID#			Method
			1-2

[illegible]

Plant	Carrs Brewery		Date	1-27-93
Location	9 can inlet (small)			
Operator	PO/MAN			
Run Number	2	Pilot Tube Coefficient	.84	
Sample Box ID#	Meter Box ID#		C Factor	
Meter ΔH @	Pre-Test Pilot Leak Check		Pre-Test Pump Leak Check	
	✓	✓	✓	✓

Air Pollution Testing, Inc.
Schematic of Stuck Cross Section

14"
1 7/8" x 1 3/8"
1 3/8" x 1 3/8"

CO2 (%)	0.0	O2 (%)	20.9
Assumed Moisture (%)	0	Barometric Pressure (inHg)	30.39
Ambient Temperature (oF)	70	Probe Material	SS
Probe Length (ft)	2	Filler Temperature (oF)	—
Probe Temperature (oF)	—	Moisture (grams)	—
Nozzle Diameter (in)	—	Start Time	—
Static Pressure (in H2O)	-1.30	Stop Time	—
Filter ID#	—	Method	1-2

Transducer Point Number	Sampling Time (minutes)	Vacuum (in Hg)	Velocity Head (in H2O)	Pressure Differential (in H2O)	Gas Volume (ft ³) Initial Volume	Stack Temp. (oF)	Probe Temp. (oF)	Filter Temp. (oF)	Inlet (oF) Gas Temp. Outlet (oF)	Condenser Temp. (oF)	Notes
1-1			.44			72					
2			1.2			72					
3			.68			72					
2-1			.56			72					
2			1.4			72					
3			.69			72					
3-1			.25			72					
2			1.1			72					
3			.23			72					
4-1			1.4			72					
2			1.5			72					
3			1.0			72					
						72					
						72					

Air Pollution Testing, Inc.
Schematic of Stack Cross Section

12" 14"

1 2 3 4

$11\frac{7}{8}" \times 13\frac{7}{8}" = 19$

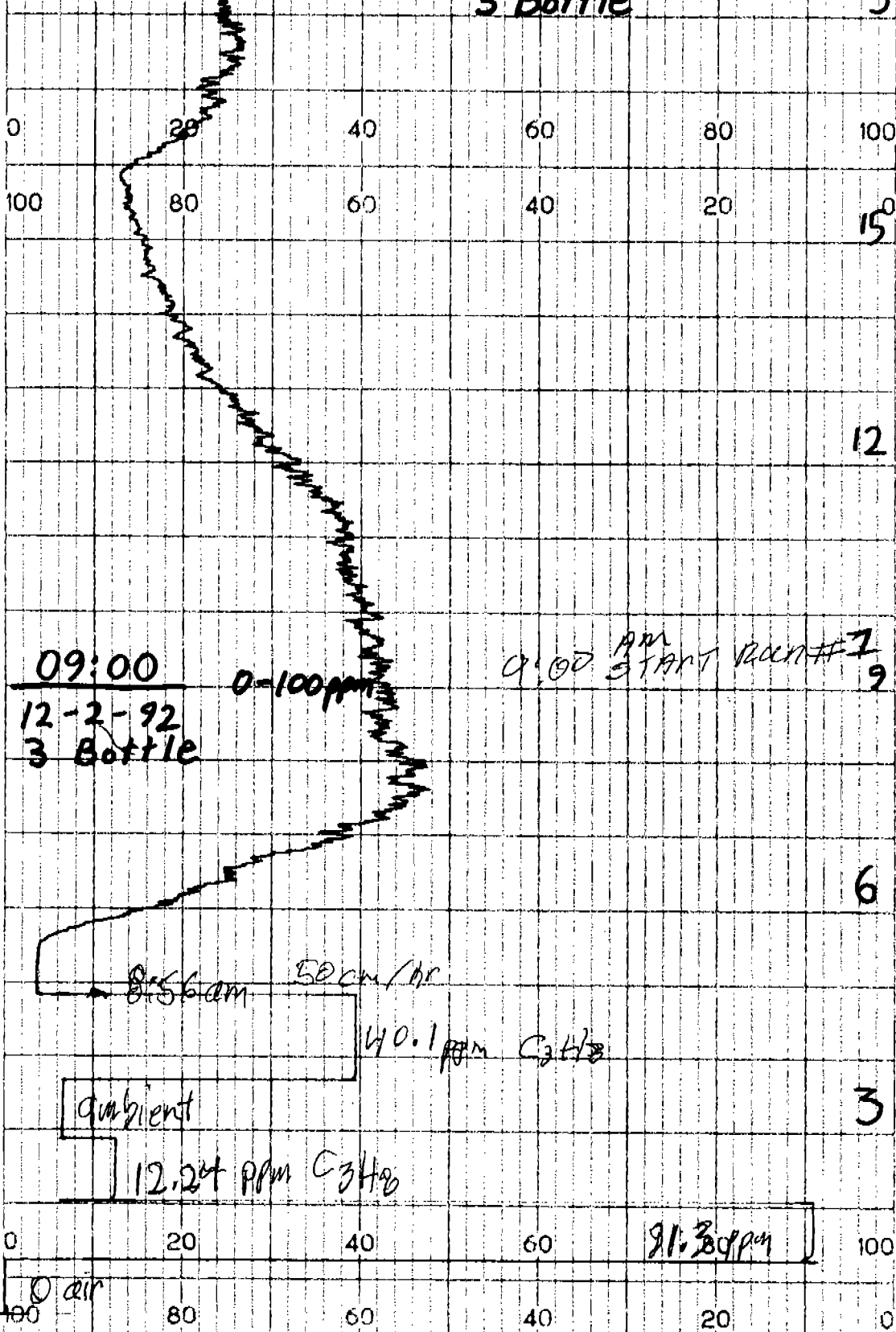
CO ₂ (%)	0.0	02 (%)	20.9
Assumed Moisture (%)	0	Barometric Pressure (inbar)	838
Ambient Temperature (oF)	70	Probe Material	SS
Probe Length (ft)	2	Filler Temperature (oF)	/
Probe Temperature (oF)	/	Moisture (grams)	/
Nozzle Diameter (in)	/	Start Time	/
Saltic Pressure (in H ₂ O)	-1.25	Stop Time	/
Filter ID#	/	Method	1-2

[illegible]

**#3 Bottle Filler
Method 25A
Strip Chart Data**

PART NO. LO/8015

PRINTED IN U.S.A.



8:45 Calibration

Method 25A
Coors Brewing Co
3 Bottle Outlet
12-2-92

PRINTED IN U.S.A.

0-100 ppm

09:36

9

12-2-92
3 Bottle

6

3

0 20 40 60 80 100
100 80 60 40 20 15°

0-100 ppm

09:24

12

12-2-92
3 Bottle

N E I S

9

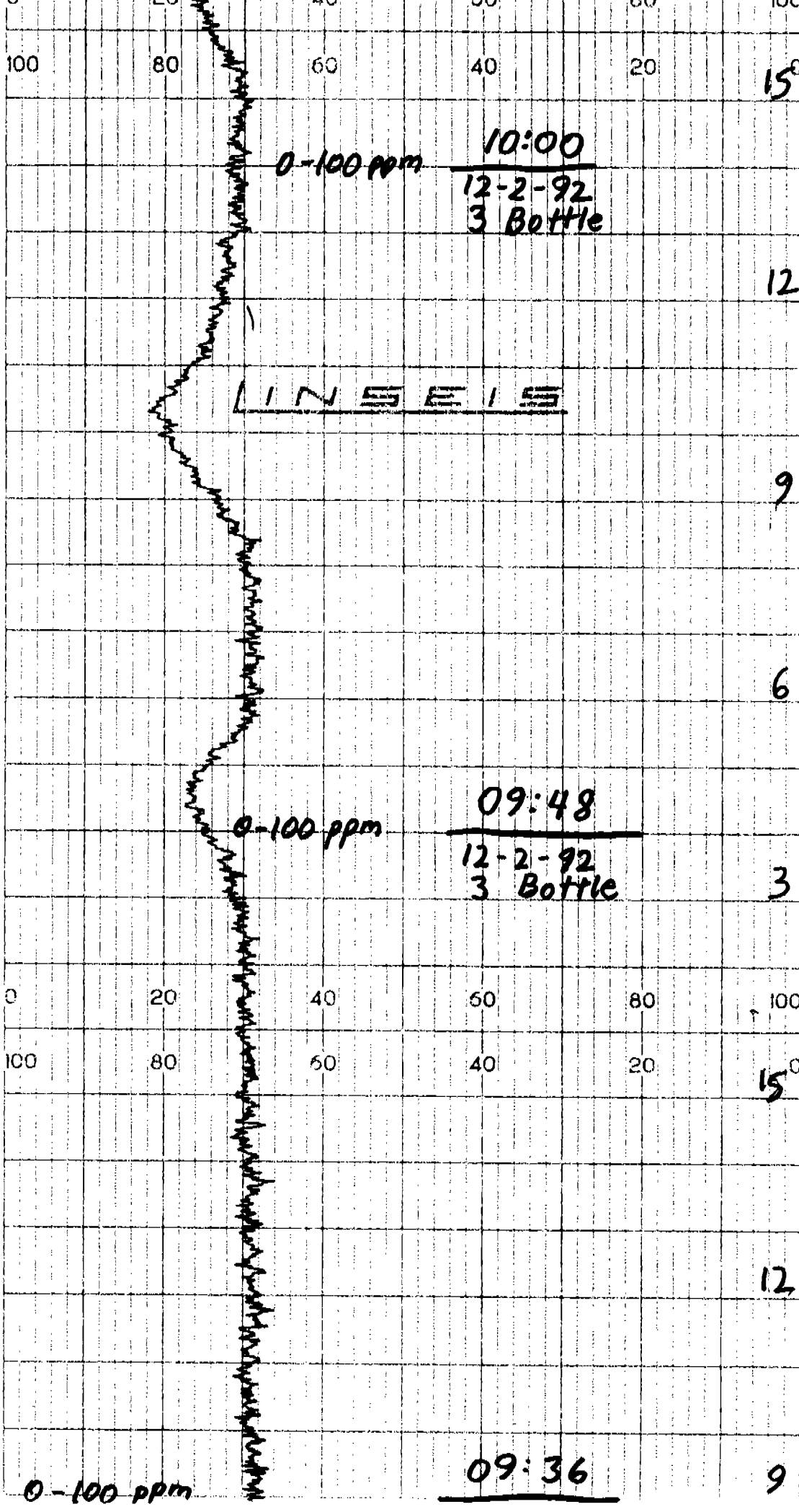
6

0-100 ppm

09:12

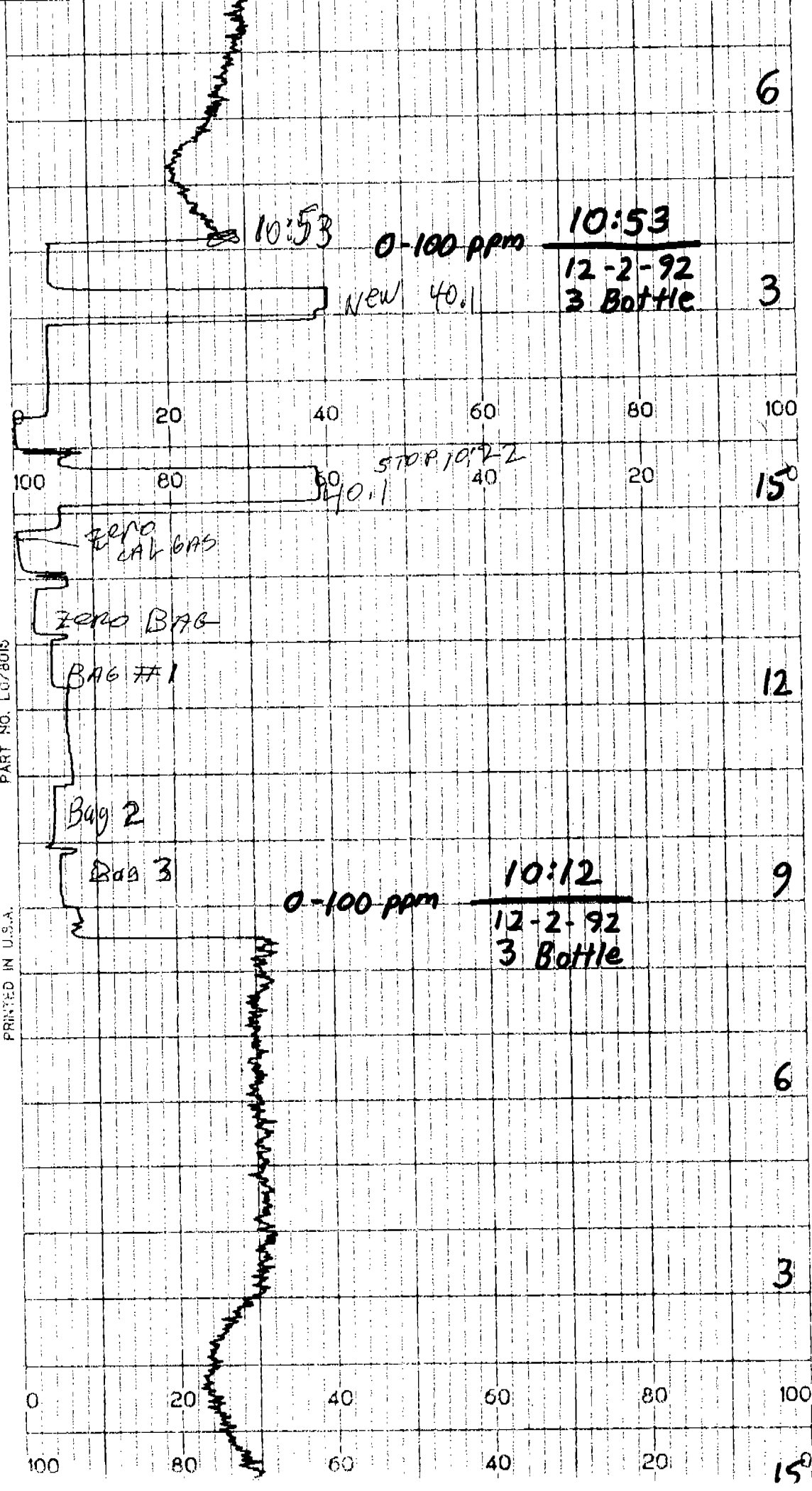
3

12-2-92
3 Bottle



PART NO. LO/8015

PRINTED IN U.S.A.



0-100 ppm

11:12

12-2-92
3 Bottle

12

9

6

3

0 20 40 60 80 100
100 80 60 40 20 15°

12

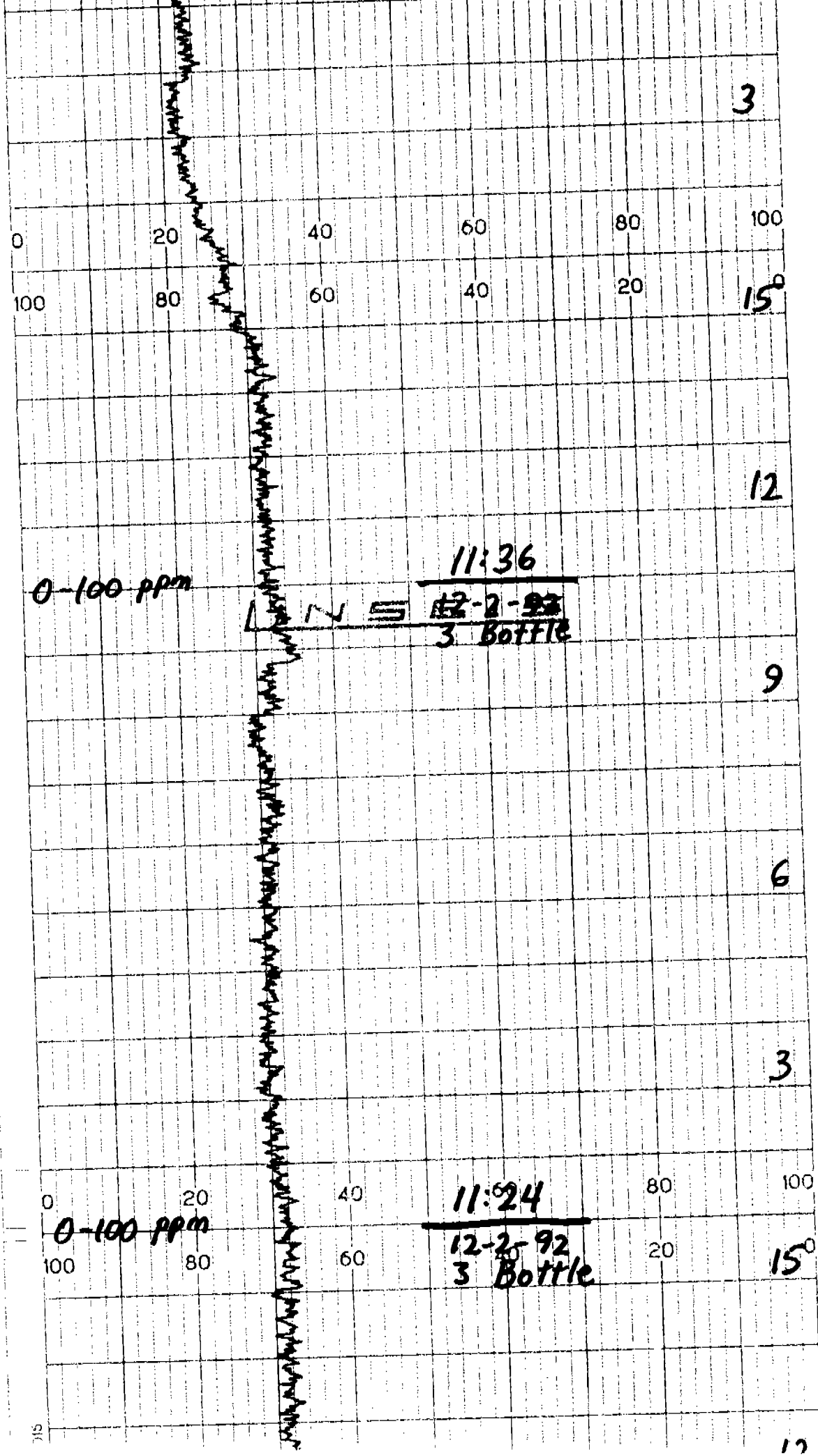
11:00

12-2-92
3 Bottle

0-100 ppm

9

6



INSEIS

9

12:30 Start Run 3

- BAG #3 ZERO
- BAG #2 ZERO
- BAG #1 ZERO

6

40.1

- ZERO

CALIBRATE 12:05

3

- BAG #3
- BAG #2
- BAG #1

0 20 40 60 80 100
100 80 STOP Run #2 40 12:00
60 12-2-92
100.25

150

0-100 ppm

11:58
12-2-92
3 Bottle

12

PART NO. LO/8015

9

PRINTED IN U.S.A.

11:48
12-2-92
3 Bottle

0-100 ppm 6

PART NO. LO/8015

PRINTED IN U.S.A.

0-100 ppm

12:48

12-2-92
3 Bottle

12

9

6

3

12:36

12-2-92
3 Bottle

0-100 ppm

100

15°

12

INSELS

9

0-100 ppm

0

20

40

13:12
12-2-92
3 Bottle

80

100

100

80

60

40

20

150

12

NEIS

9

0-100 ppm

13:00

12-2-92
3 Bottle

6

3

0

20

40

60

80

100

LINSEIS

9

40.6 ppm

0 air

6

Bag 3

Bag 2

Bag 1

3

13:31 Stop Run 3

0 20 40 60 80 100
100 80 60 40 20 15°

13:24

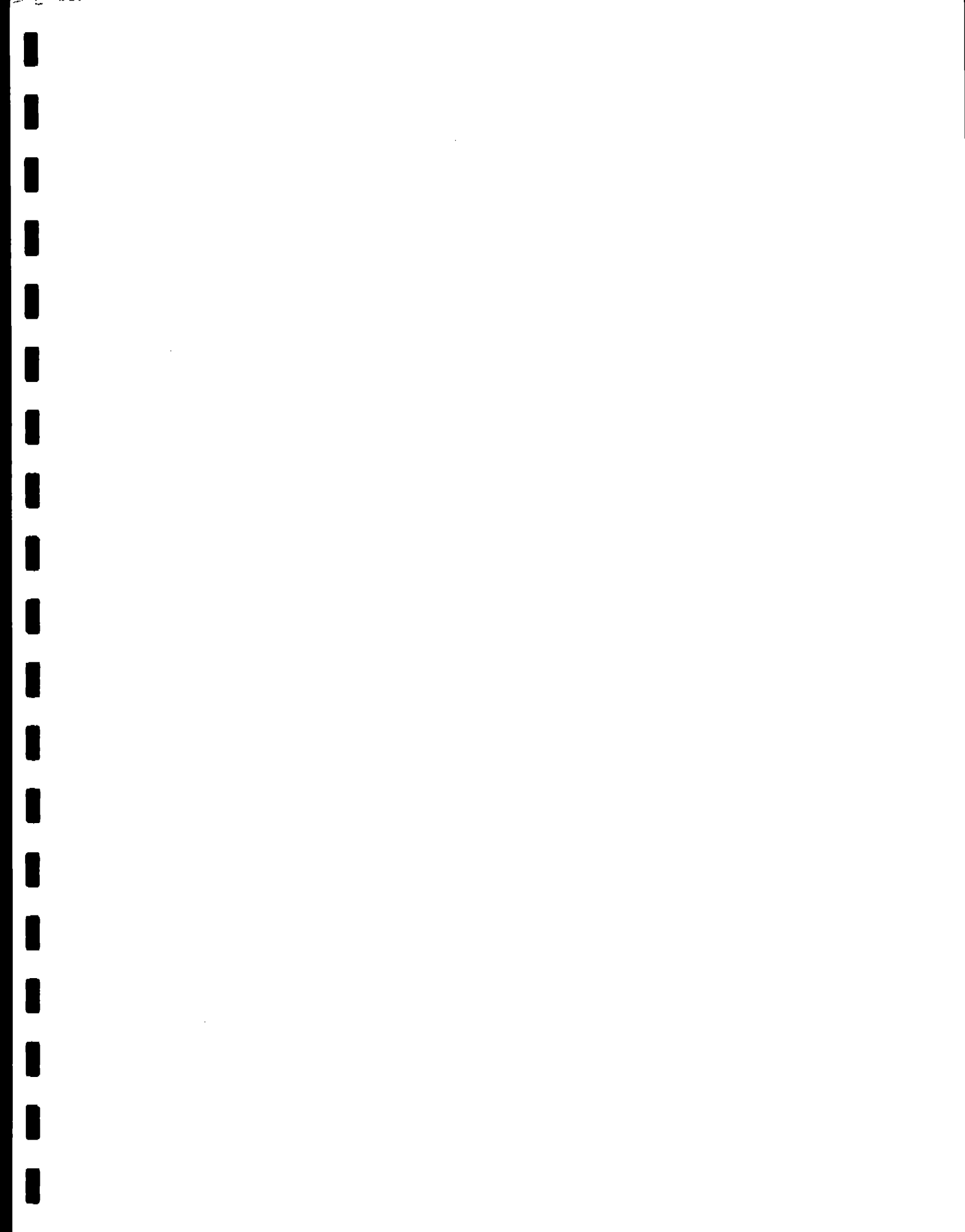
12-2-92
3 Bottle

0-100 ppm 12

9

PART NO. LO/8015

PRINTED IN U.S.A.



**#5 Can Filler
Method 25A
Strip Chart Data**

PRINTED IN U.S.A.

0-200 ppm

0 - 20 Volts

4:58 start Run 1

40, f.p.m

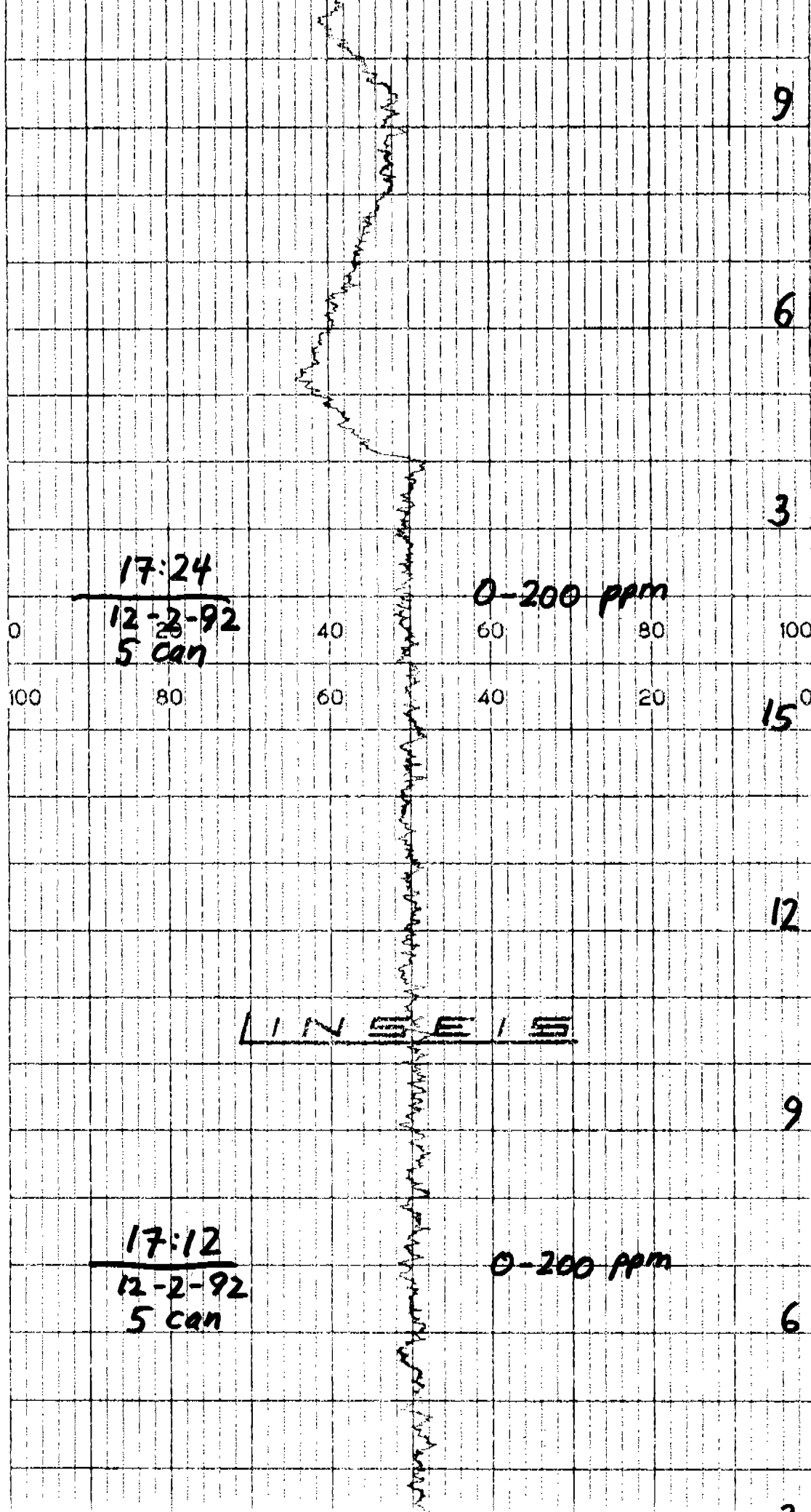
丁巳年

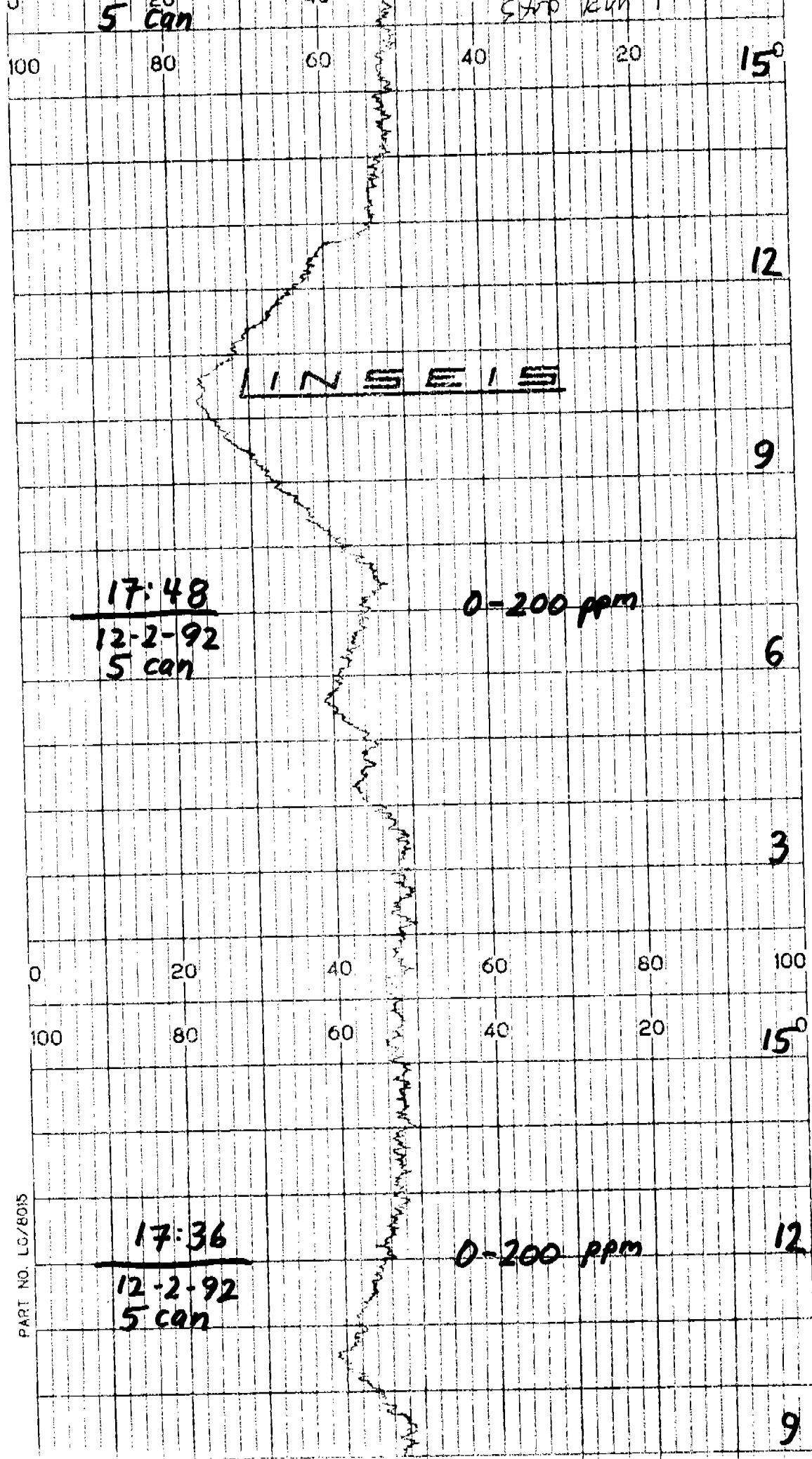
7420

CALIBRATION	15.15
	12-2-92

Coors Brewing Co
5 Can
12-2-92
VOC

PRINTED IN U.S.A.





PART NO. LG/8015

0-200 ppm

18:24

12-2-92

5 can

6

3

0 20 40 60 80 100
100 80 60 40 20 15°

PART NO. LO/BOIS

0-200 ppm

18:12

12-2-92

5 can

12

9

PRINTED IN U.S.A.

40005

Run #2
START

18:06

12-2-92

6

(Bgd #1)

91.3 ppm C_3H_8

3

18:00

12-2-92

5 can

40

6:00 PM

START

0-200 ppm

Run 1

100

18:48
12-2-92
5 can

0-200 ppm

12

9

6

3

0-200 ppm

0

20

40

100

80

60

18:36

12-2-92
5 can

80

100

40

20

15

12

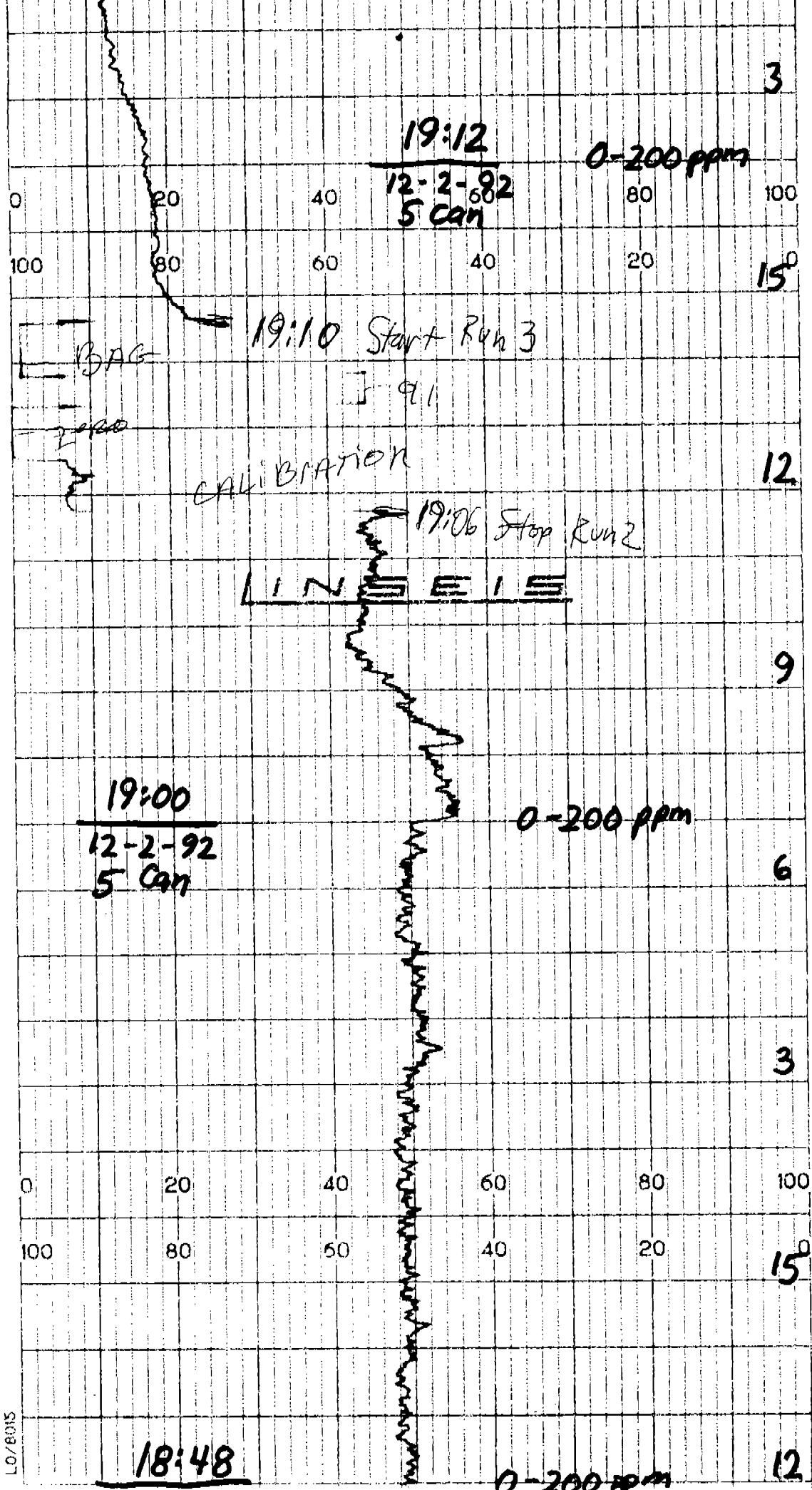
175 E 15

9

0-200 ppm

18:24

12-2-92



LO/BDIS

L I N E I S

9

0-200 ppm

19:36

12-2-92

5 can

6

3

0 20 40 60 80 100
100 80 60 40 20 15°

PART NO. LO/8015

0-200 ppm

19:24

12-2-92

5 can

12

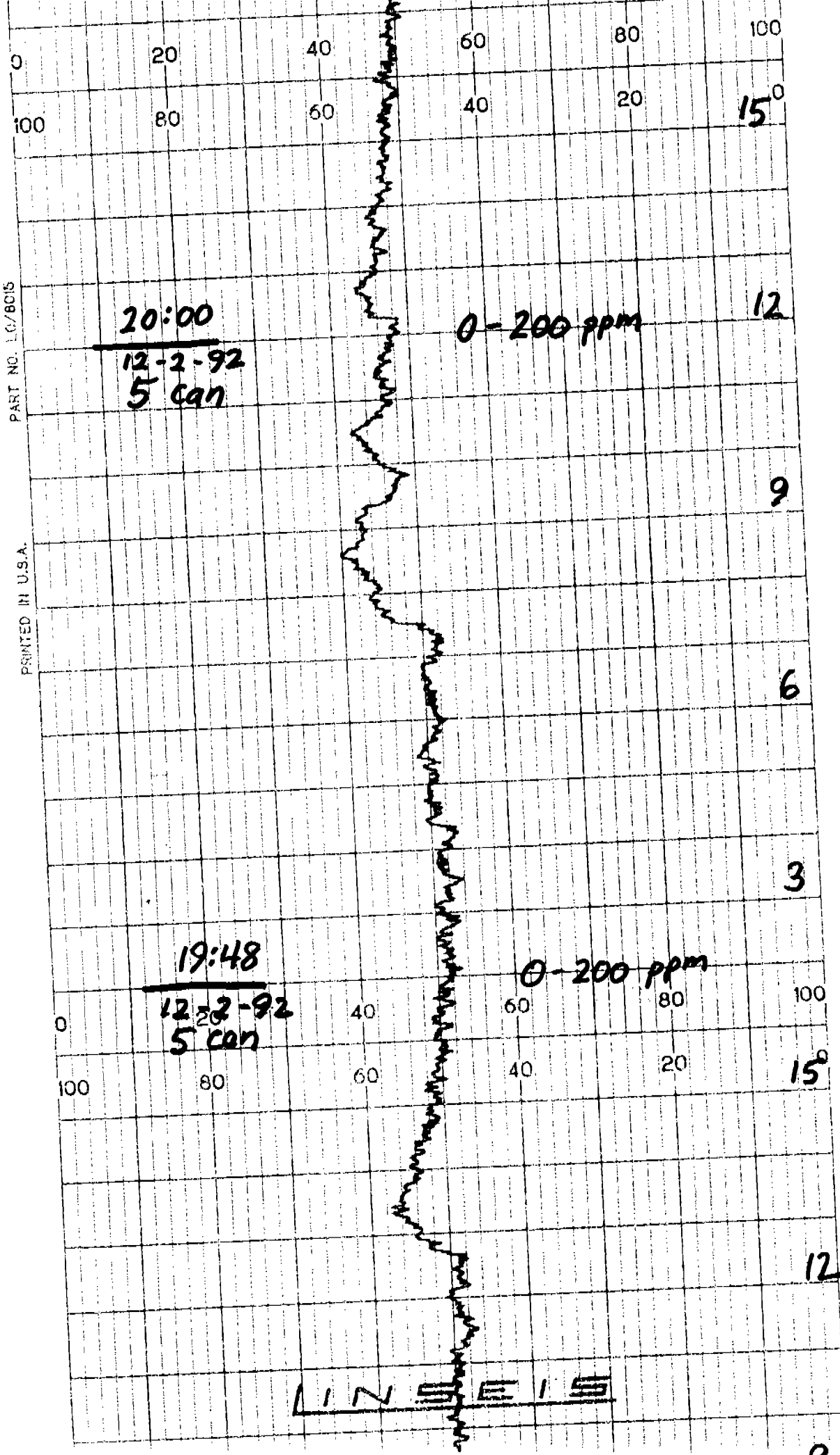
9

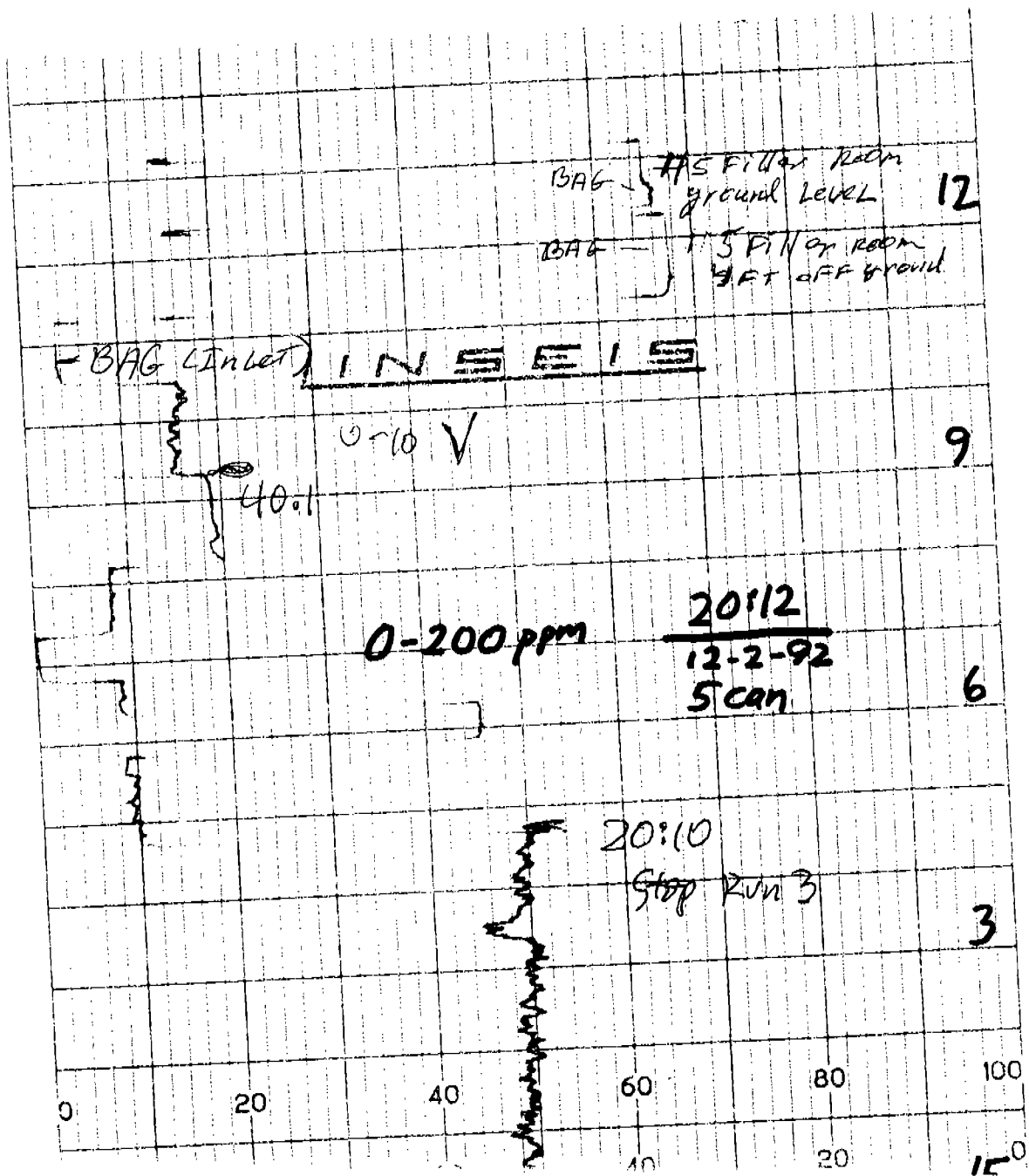
PRINTED IN U.S.A.

6

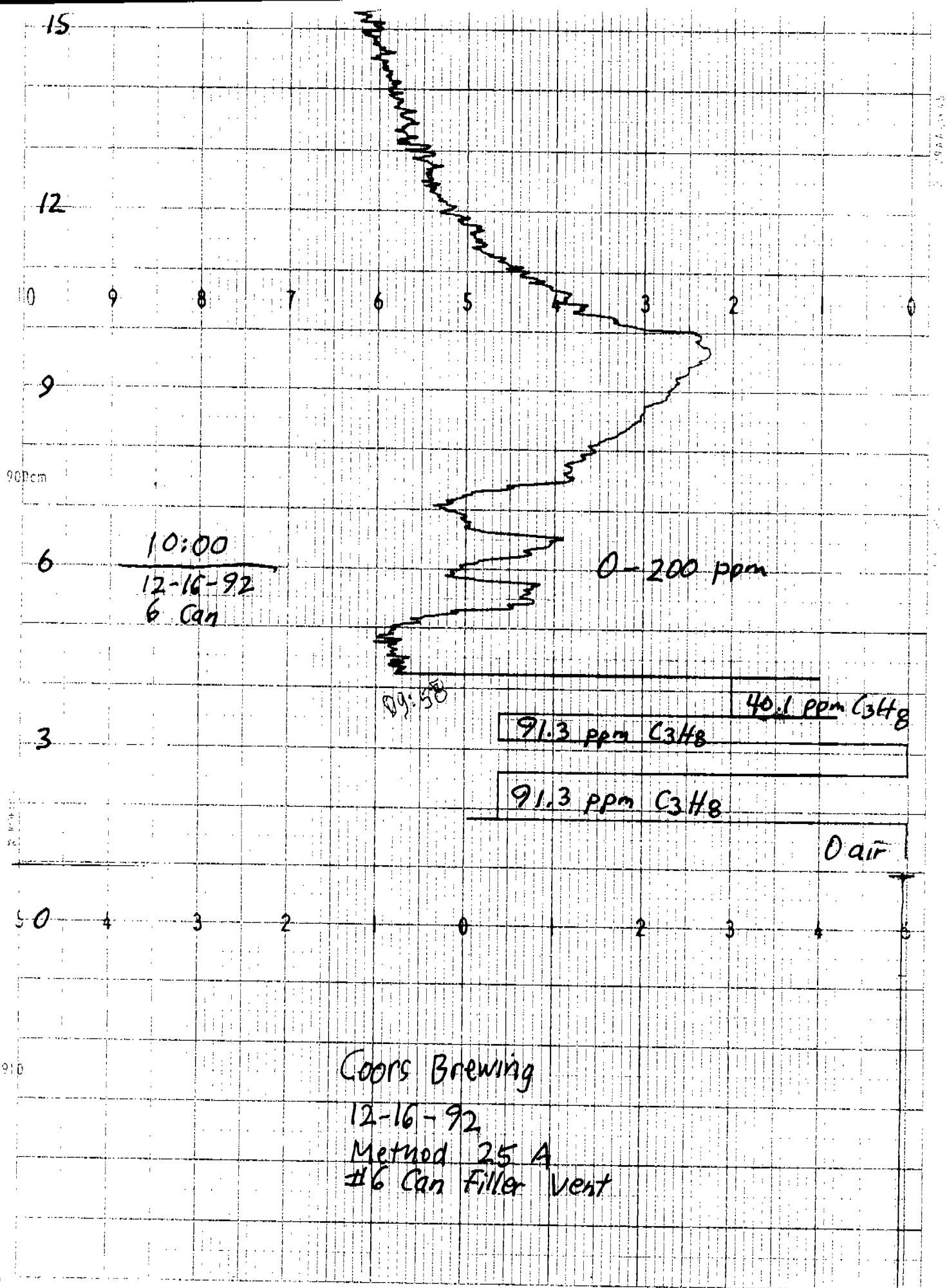
PART NO. LC/8015

PRINTED IN U.S.A.





**#6 Can Filler
Method 25A
Strip Chart Data**



KORUSAI

6

10:30

12-16-92

6 Can

0-200 ppm

3

5

4

3

2

1

0

1

2

3

4

5

15

12

12

9

6

2

3

4

5

6

7

8

9

10:15

12-16-92

6 Can

0-200 ppm

3

15

15

12

9

0

1

2

3

4

5

6

7

8

9

6

10:45

12-16-92

6 cm

0 - 200 ppm

3

860

15

12

9

8

7

6

5

4

3

2

1

9

870

6

15

Room
BagInlet #1
BagInlet #2
Bag

12

91.3 ppm C_3H_8

0 air

9

91.3 ppm C_3H_8

840

6

11:00

12-16-92

6 can₃

0-200 ppm

15

8000

12

7

6

3

15

820

12

9

6

3

11:30
12-16-92
6 can

0-200 ppm

11420

91.3 ppm C3H8

0 air

15

12

9

6

3

11:45

12-16-92

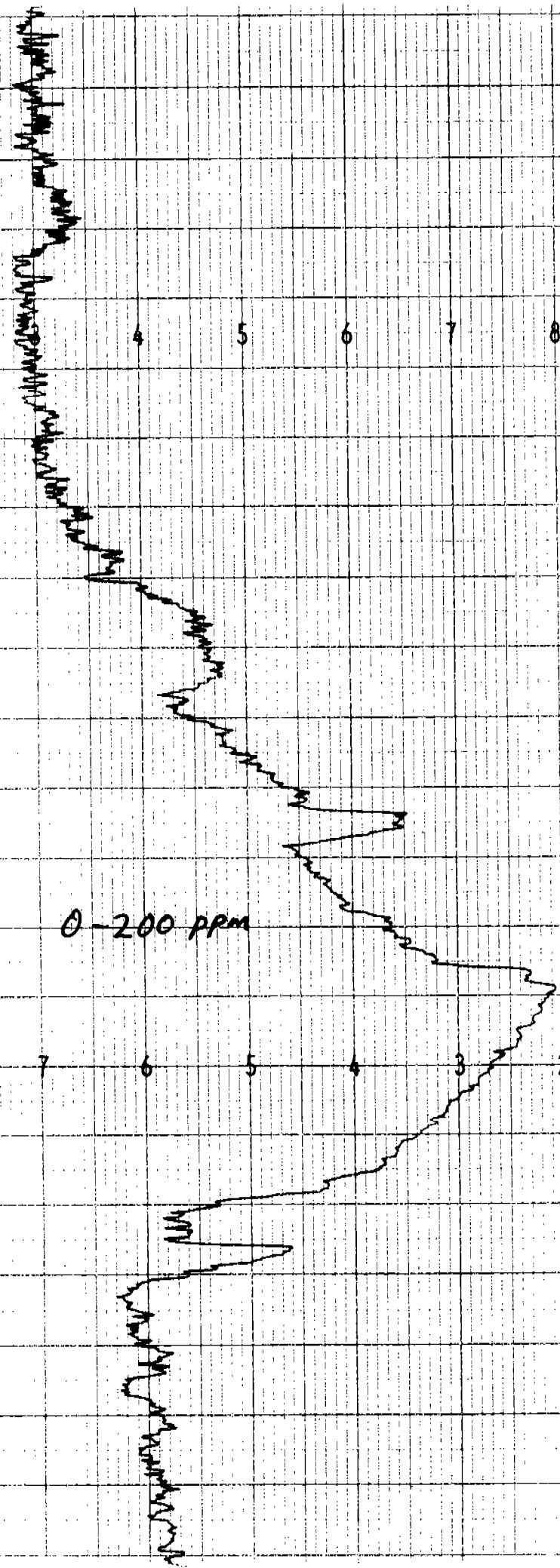
6 Can

0-200 ppm

15

12

9



3

770

12:15

12-16-92

6 can

0-200 ppm

15

12

9

6

4

3

2

0

1

2

3

4

5

3

12:00

12-16-92

6 can

0-200 ppm

15

Inlet #2 Bag

Inlet #1 Bag

91.3 ppm C₃H₈

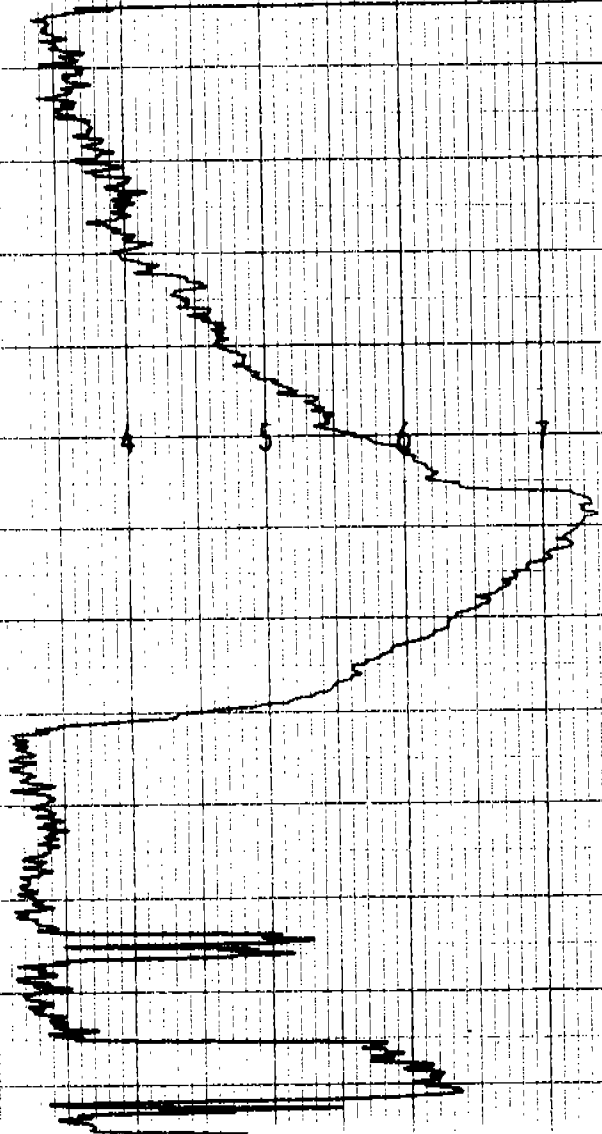
0 air

0 air

91.3 ppm C₃H₈

12:30
12-16-92
6 can

0-200 ppm



13:15

12-16-92

6 Can

0-200 ppm

15

12

9

6

3

13:00

12-16-92

6 Can

0-200 ppm

12:58

91.3 ppm C₃H₈

0 air

Room Bag

Inlet Bag 2

12

6

3

13:30

12-16-92

6 can

0-200 ppm

15

12

9

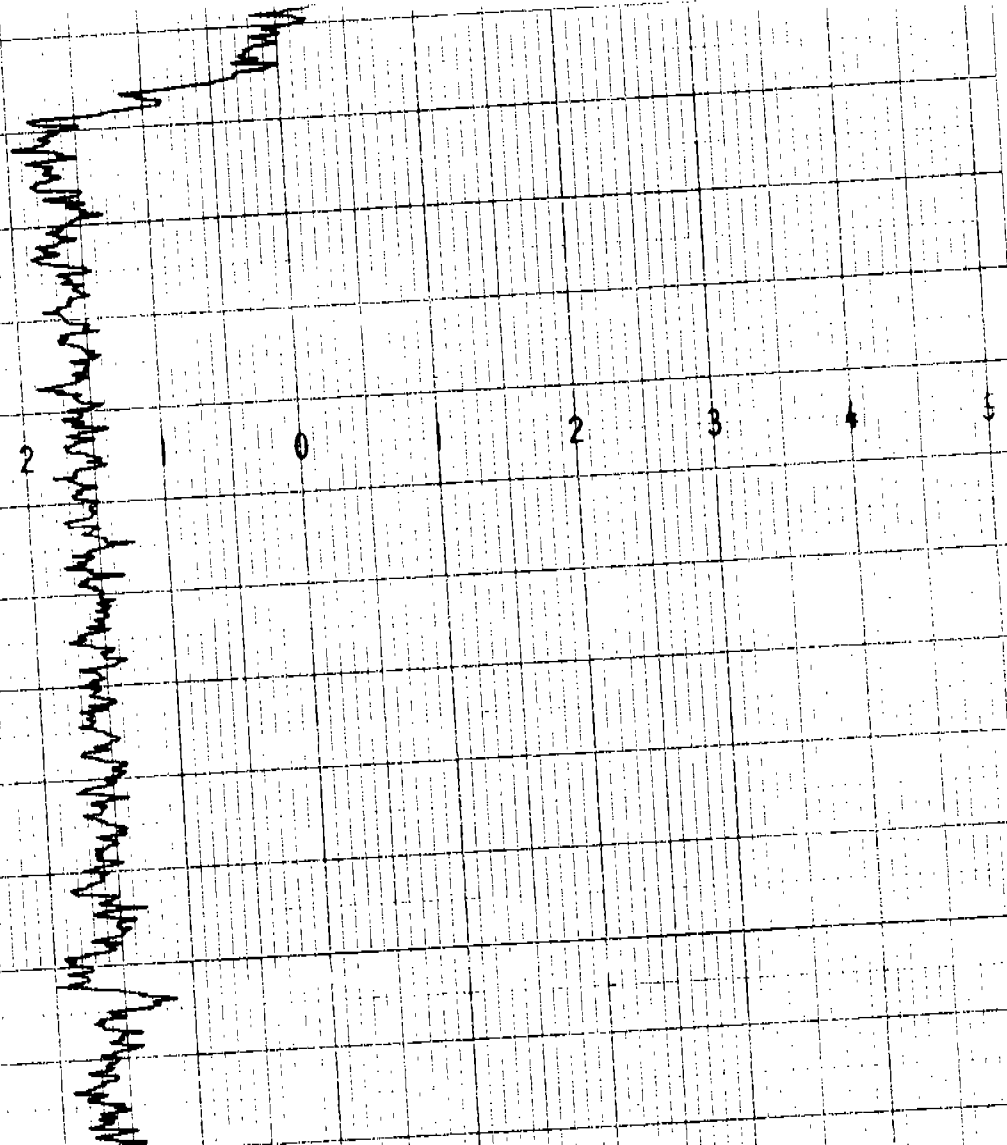
6

3

13:15

12-16-92

0-200 ppm



13:45

12-16-92

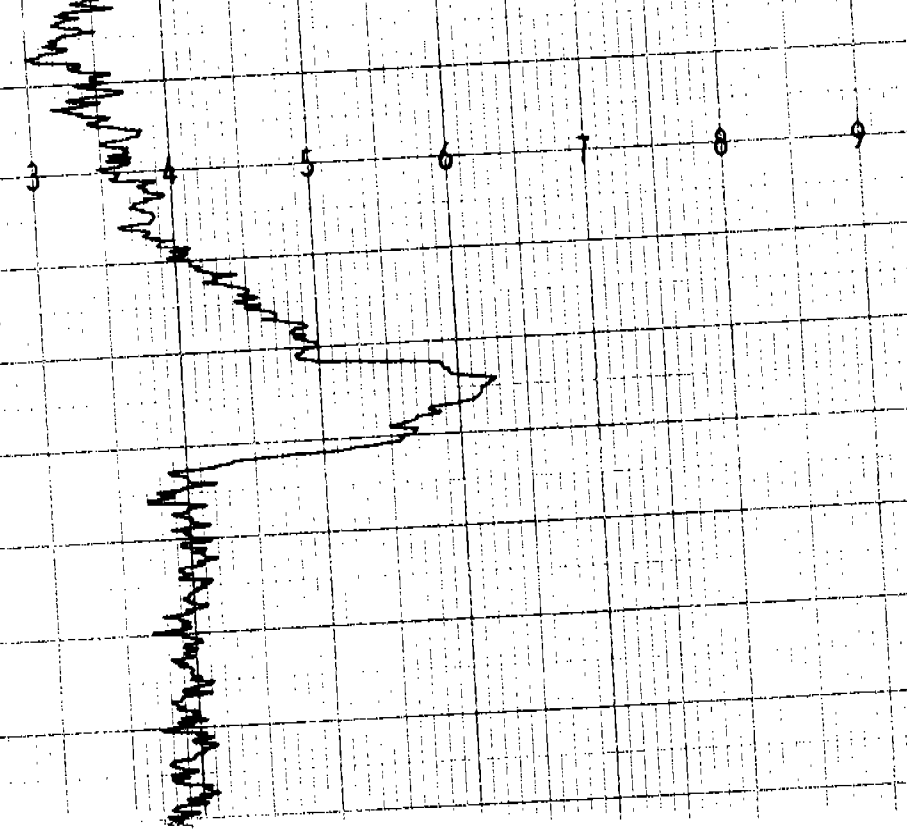
6 can

0-200 ppm

15

12

9



15

12.24

ppm
 C_3H_8

12

40.1 ppm C_3H_8

Room Bag

9

Inlet # 2
Bag

Inlet # 1
Bag

6

0 air

91.3 ppm C_3H_8

3

14:00

12-16-92

6 Can

0-200 ppm

15

**#9 Can Filler
Method 25A
Strip Chart Data**

6

08:00

12-3-92

9 Can

0-200 ppm

3

0 20 40 60 80 100

100 80 60 40 20 150

PART NO. LO/BUS

7:34

7:30 Started Cleaning

12

07:30

12-3-92

9 Can

0-200 ppm

9

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40.1

START run #1 7:23 Am

6

91.3

ZERO AIR

Reelwork Speed 20 cm per Hour

3

20 VOLTS

200PS 9 CAN FILTER

7:15

12-3-92

CALIBRATION

0 20 40 60 80 100

100 80 60 40 20

12

09:00
12-3-92
9 Can

0-200 ppm

9

6

3

0 20 40 60 80 100

100

80

08:30

12-3-92
9 Can

40

20

0-200 ppm

15

12

LINE IS

9

6

3

0 20 40 60 80 100

100 80 10:00 40 20 15°

12-3-92
9 can

0-200 ppm

12

L I N E I S

9

6

09:30

12-3-92
9 can

0-200 ppm

3

0 20 40 60 80 100

100 80 09:20 TB 40 20 15°

11:15 8-10-74

L I N E I S

9

6

11:00

0-200 ppm

12-3-92
9 can

3

0 20 40 60 80 100
100 80 60 40 20 15°

PART NO. LO/8015

12

10:30

0-200 ppm

12-3-92
9 can

9

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6

2

PART NO. LO/6015

PRINTED IN U.S.A.

0 20 40 60 80 100
100 80 60 40 20 15°

12:00
12-3-92
9 can

0-200 ppm

12

9

6

3

0 20 40 60 80 100
100 80 60 40 20 15°

11:30
12-3-92
9 can

0-200 ppm

11:26
10.1

0

11:20 cal

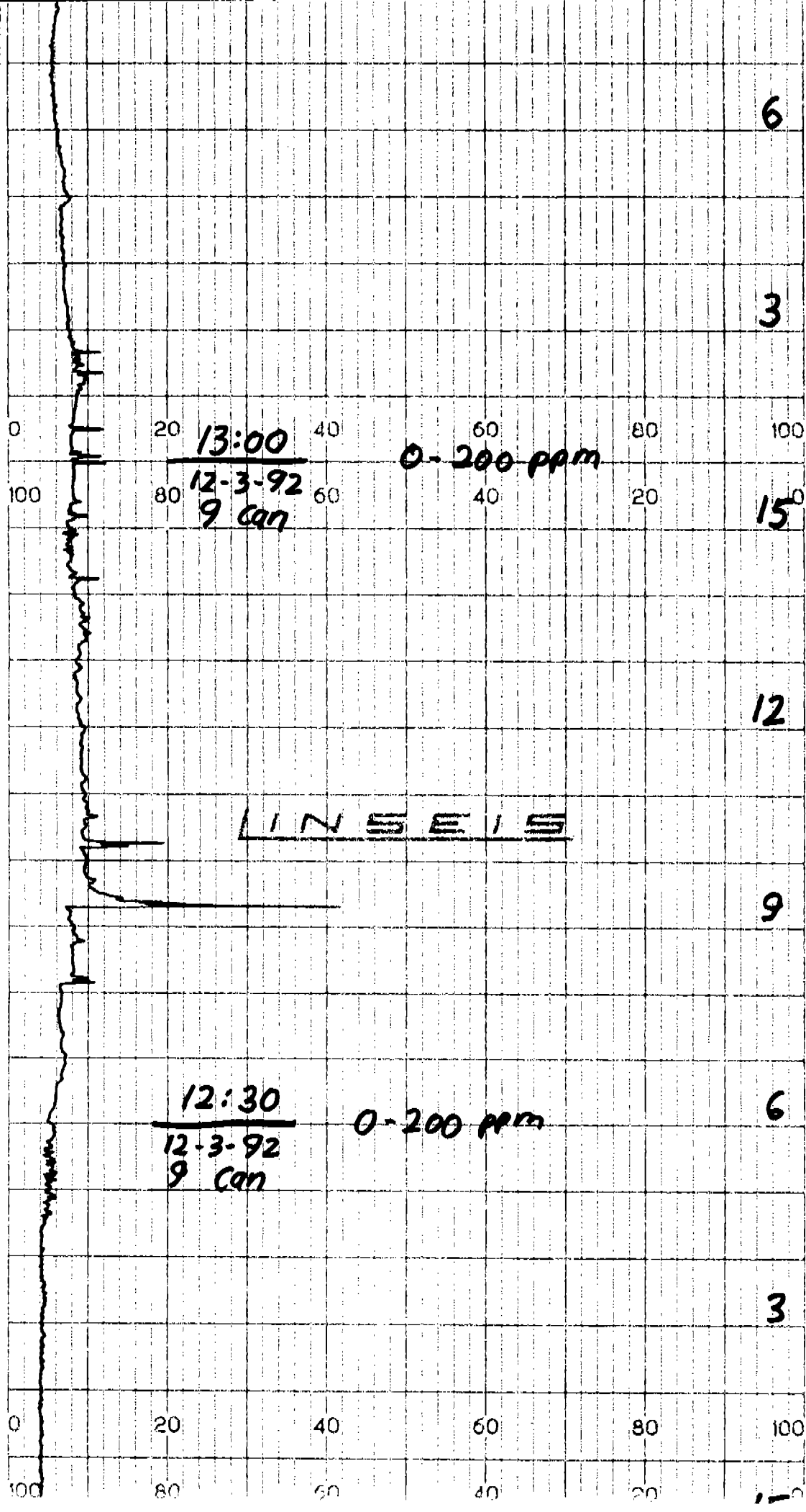
15°

12

LINE 15

11:15 6.2

9



12

L I N S E I S

9

14:00

12-3-92

9 can

0-200 ppm

6

3

0 20 40 60 80 100
100 80 60 40 20 15°

12

13:30

12-3-92

9 can

0-200 ppm

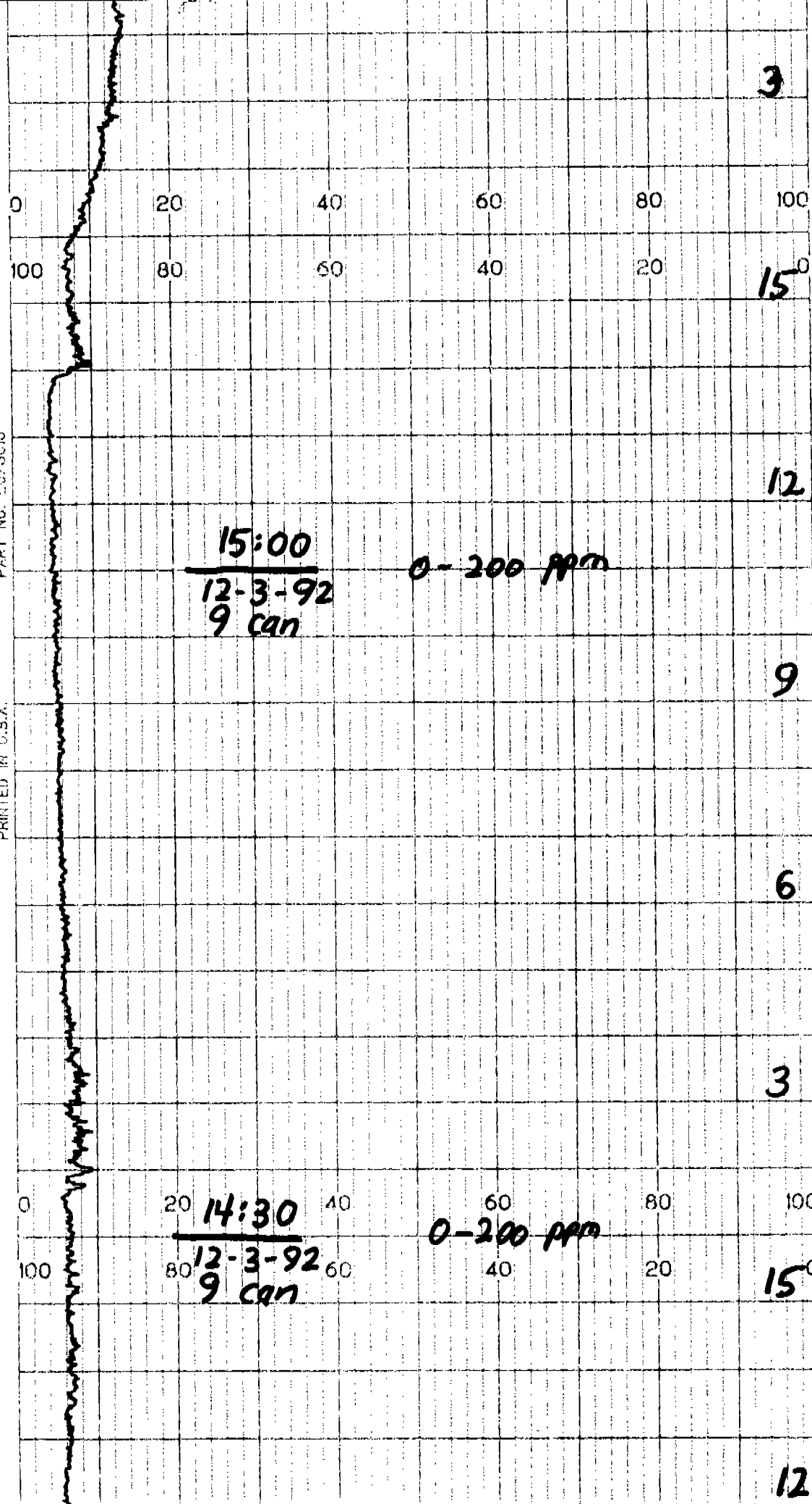
9

PART NO. LO/9015

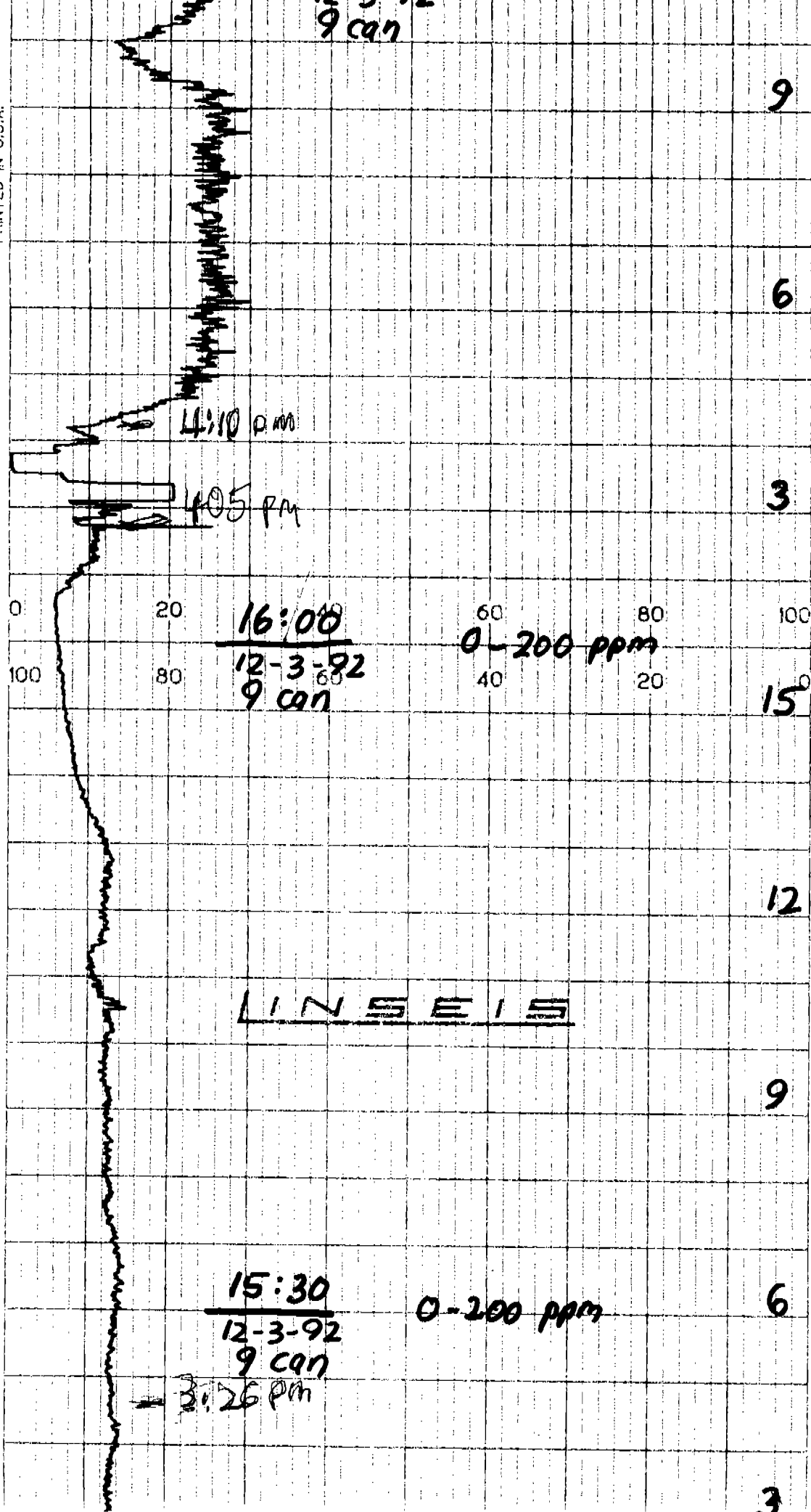
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PART NO. LC/SCIS

PRINTED IN U.S.A.



PRINTED IN U.S.A.



100

80

17:30
12-3-92
9 can

40

0-200 ppm

20

15°

12

LINE 15

9

17:00

12-3-92
9 can

0-200 ppm

6

3

0

20

40

60

80

100

100

80

60

40

20

15°

PART NO. LO/BOIS

12

16:30

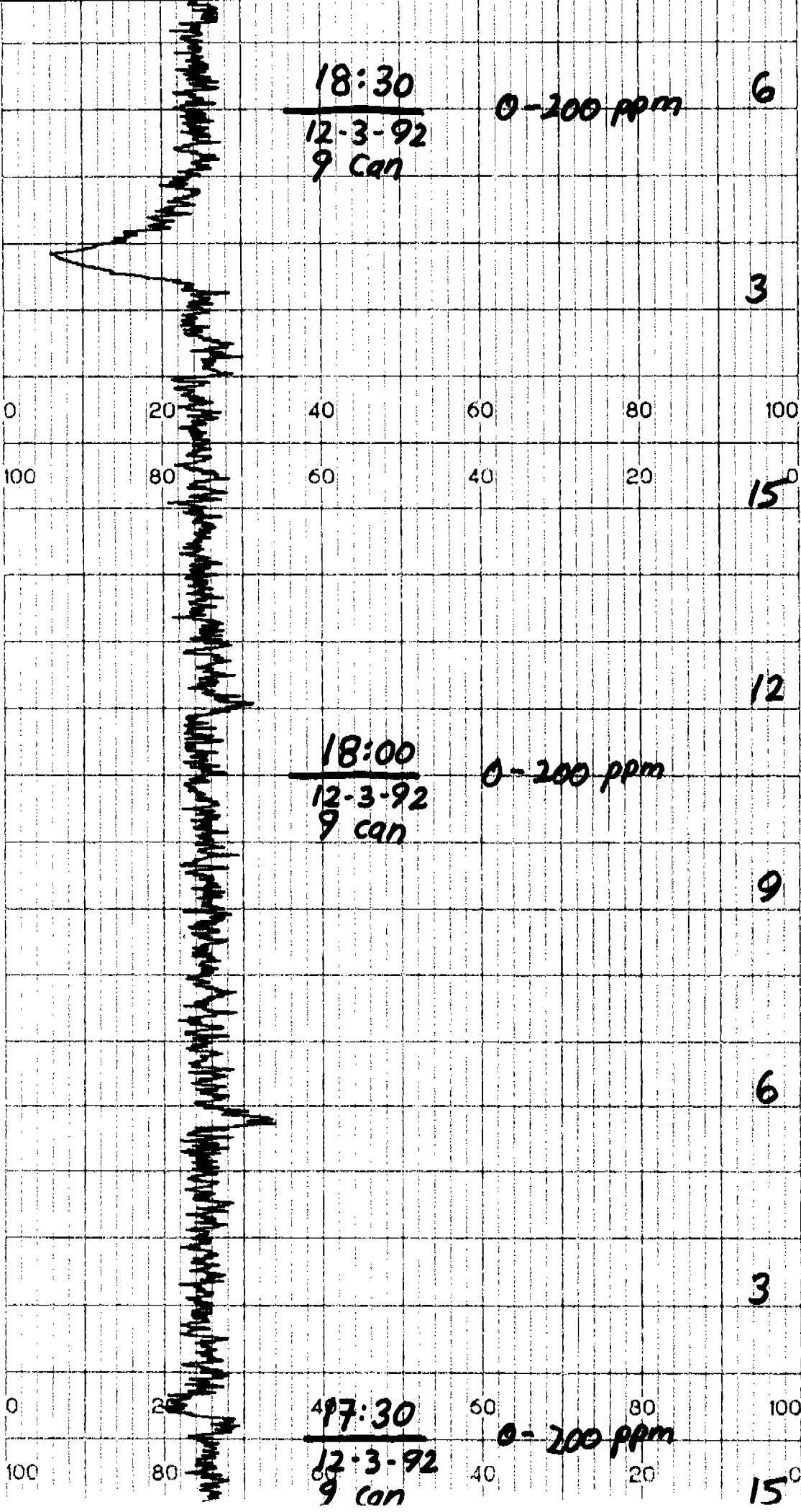
12-3-92
9 can

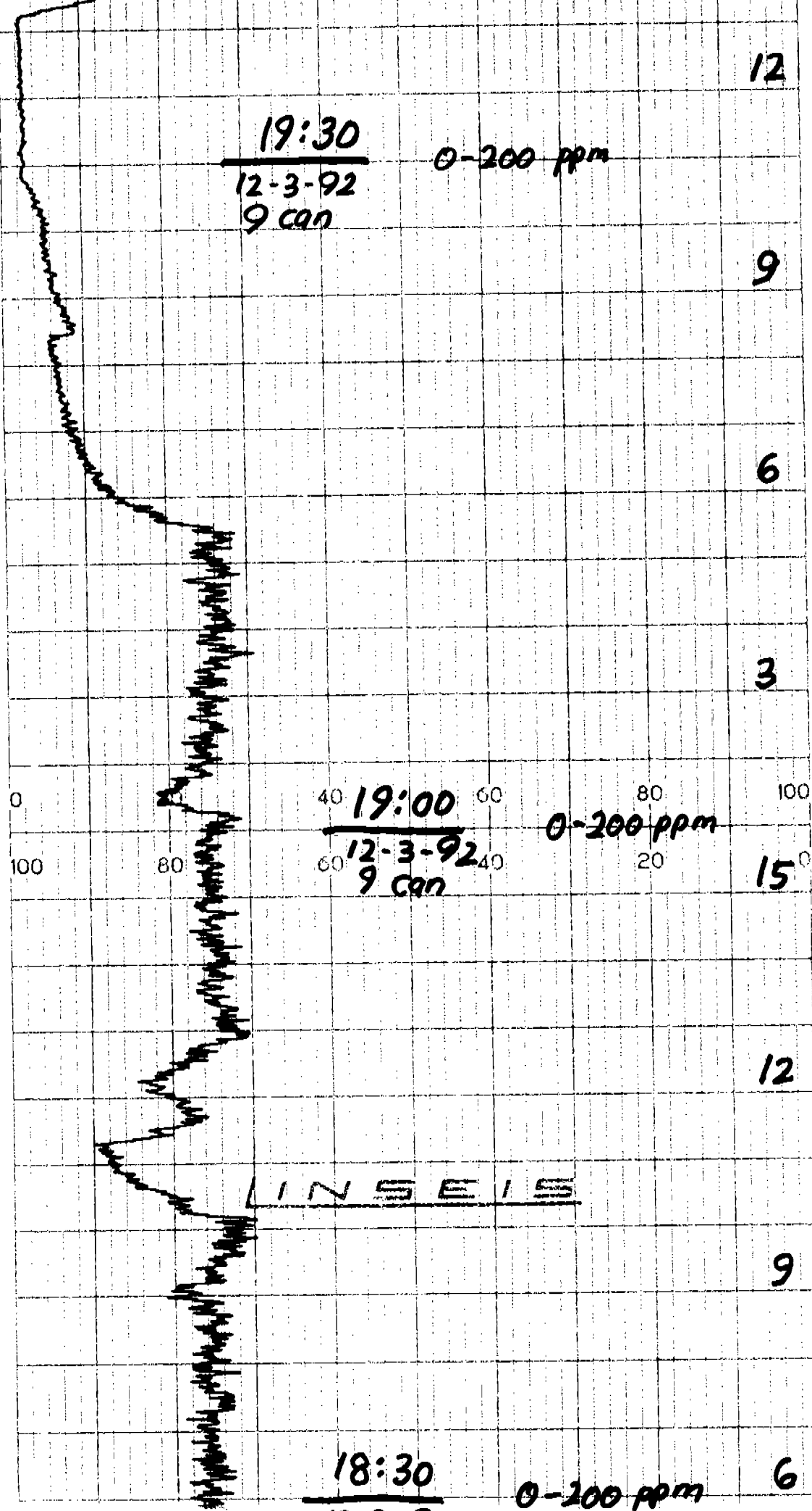
0-200 ppm

9

PART NO. LO/6015

PRINTED IN U.S.A.





12

19:30
12-3-92
9 can

0-200 ppm

9

6

3

19:00
12-3-92
9 can

0-200 ppm

15°

12

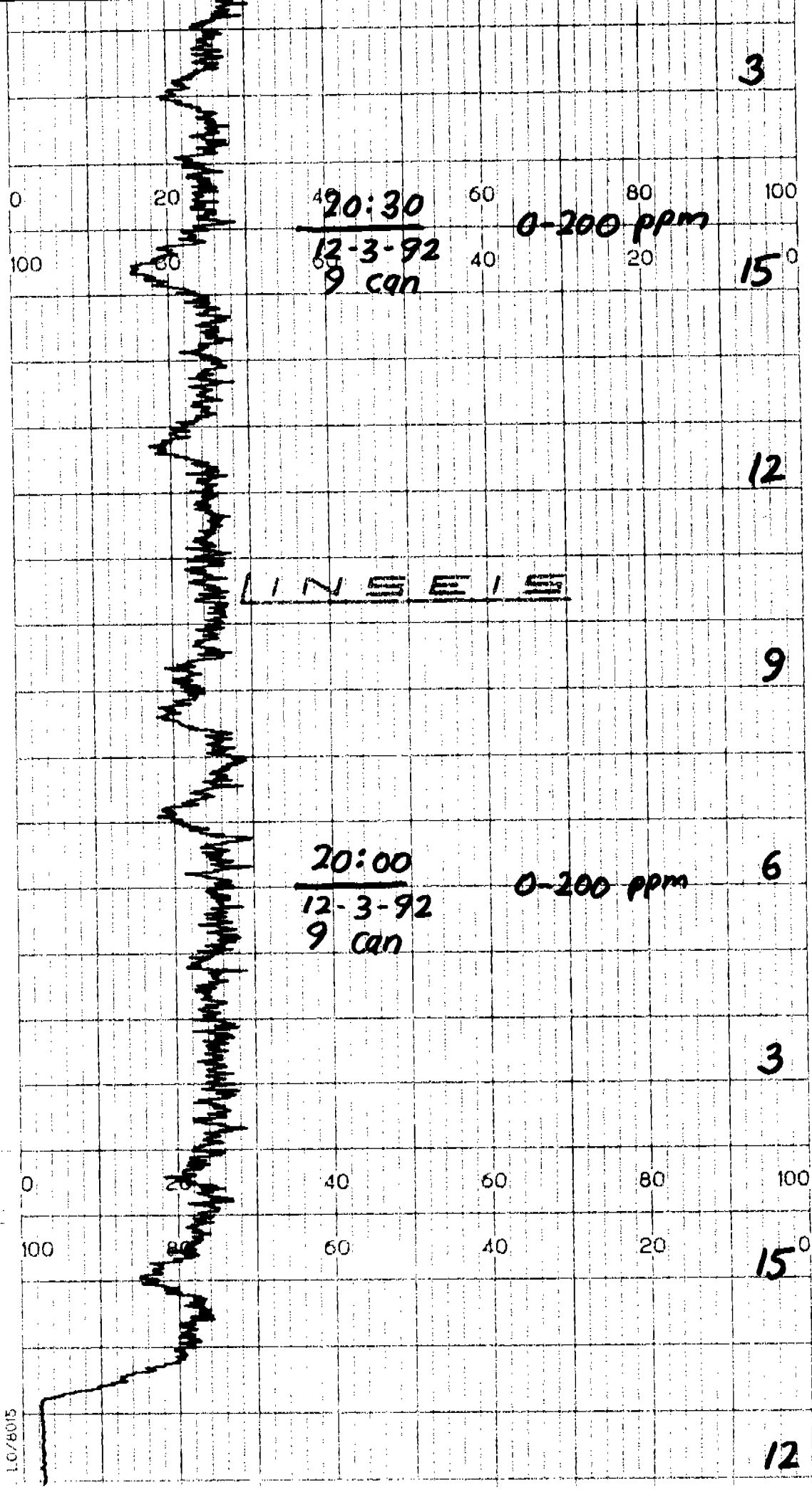
INSEIS

9

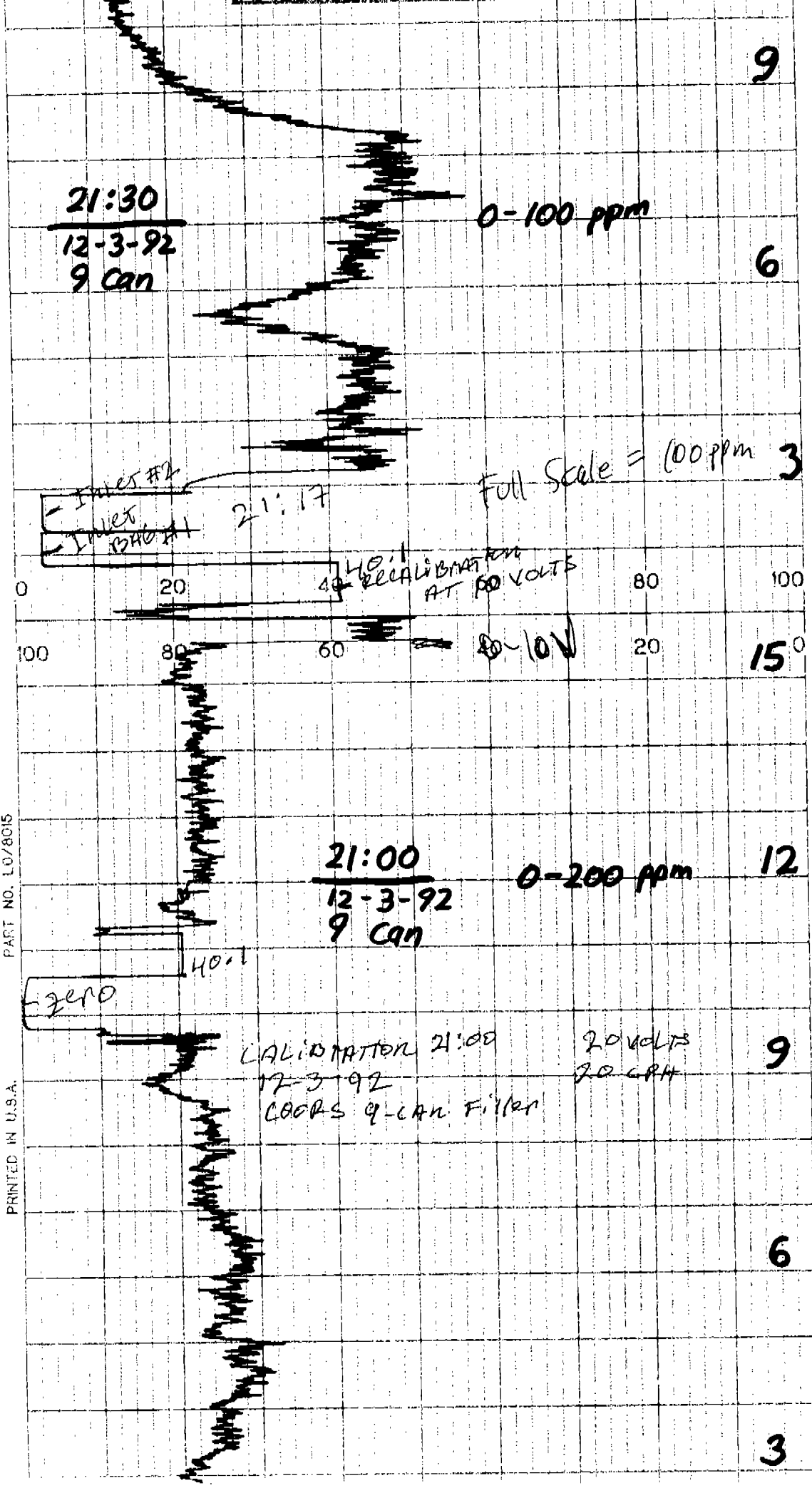
18:30

0-200 ppm

6



PART NO. 10/8015
PRINTED IN U.S.A.



21:30
12-3-92
9 Can

0-100 ppm

Full Scale = 100 ppm

Inter #2
Inter BNC #1

21:17

40.1
RECALIBRATION
AT 10 VOLTS

80-10V

21:00
12-3-92
9 Can

0-200 ppm

zero

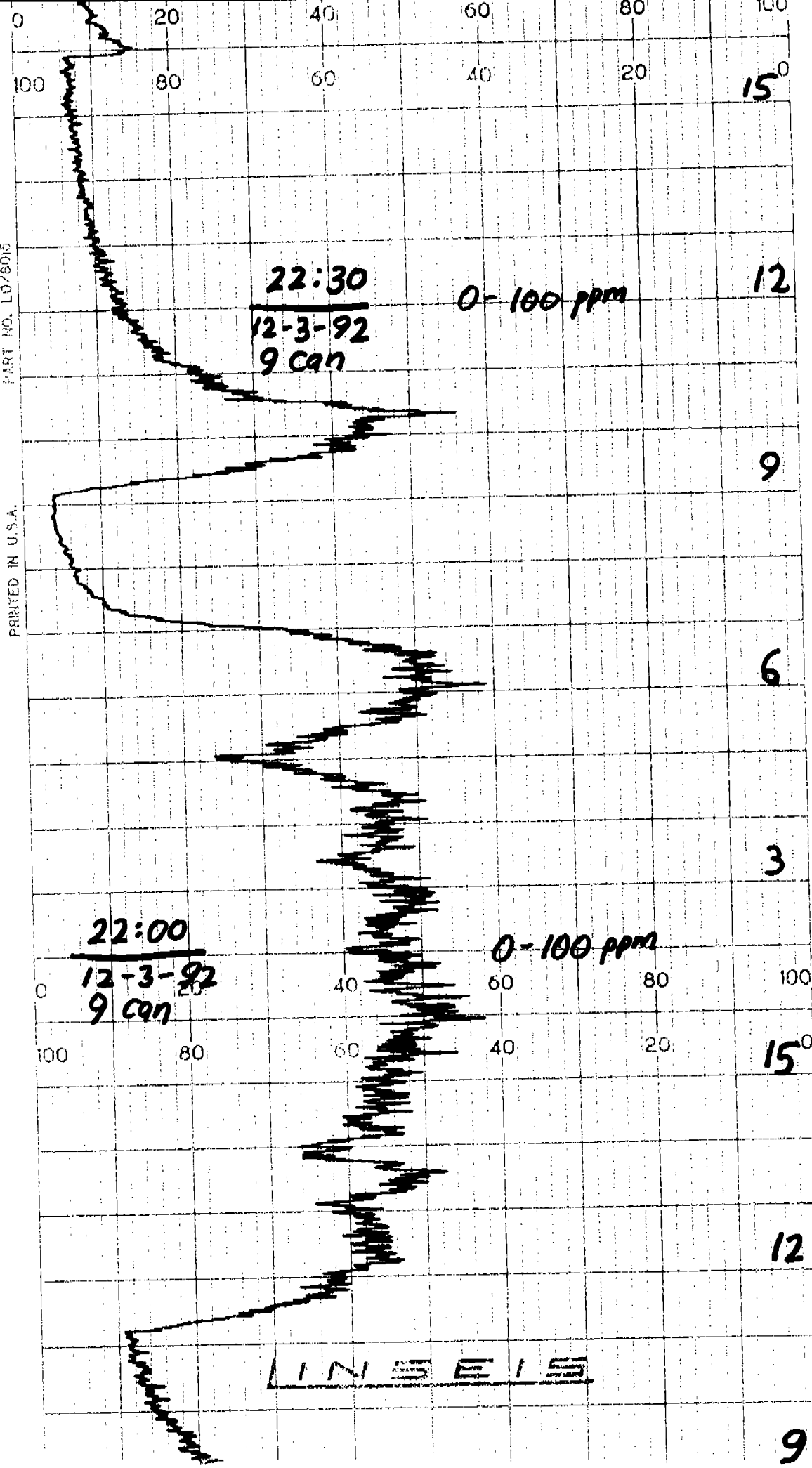
40.1

CALIBRATION 21:00
12-3-92
COORS 9-CAN Filter

20 VOLTS
20 GPH

PART NO. L078015

PRINTED IN U.S.A.



12

9

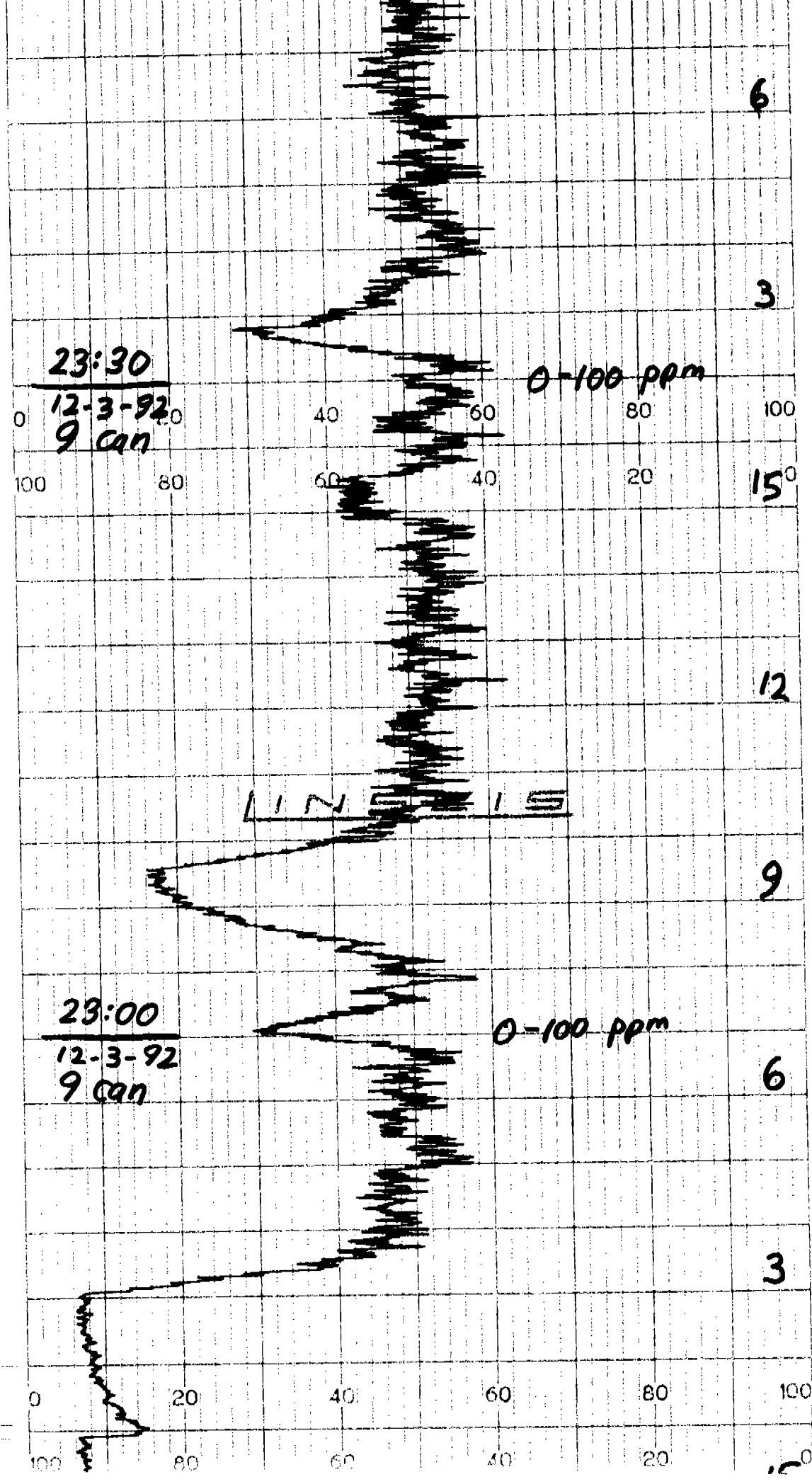
6

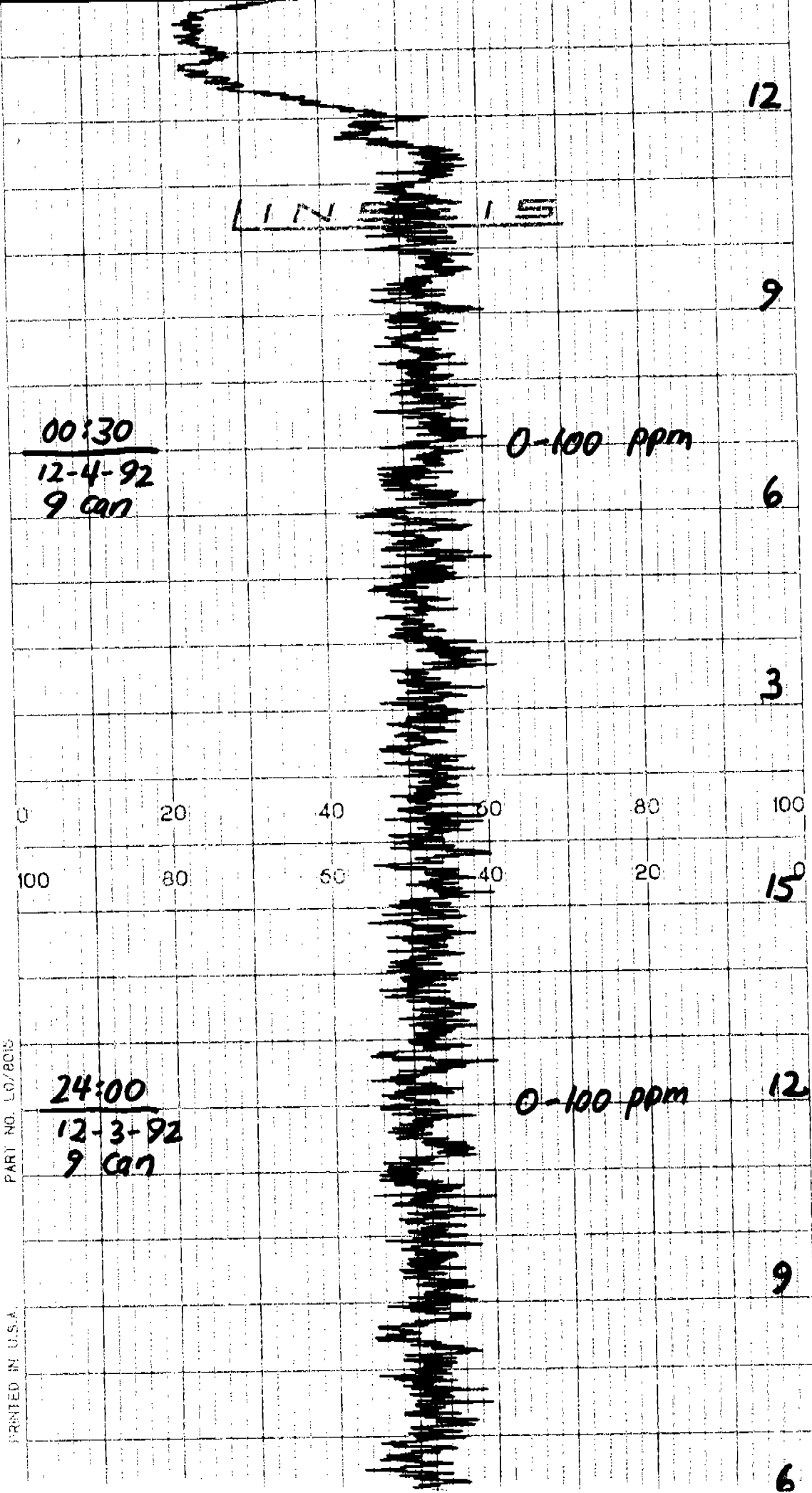
3

15°

12

9



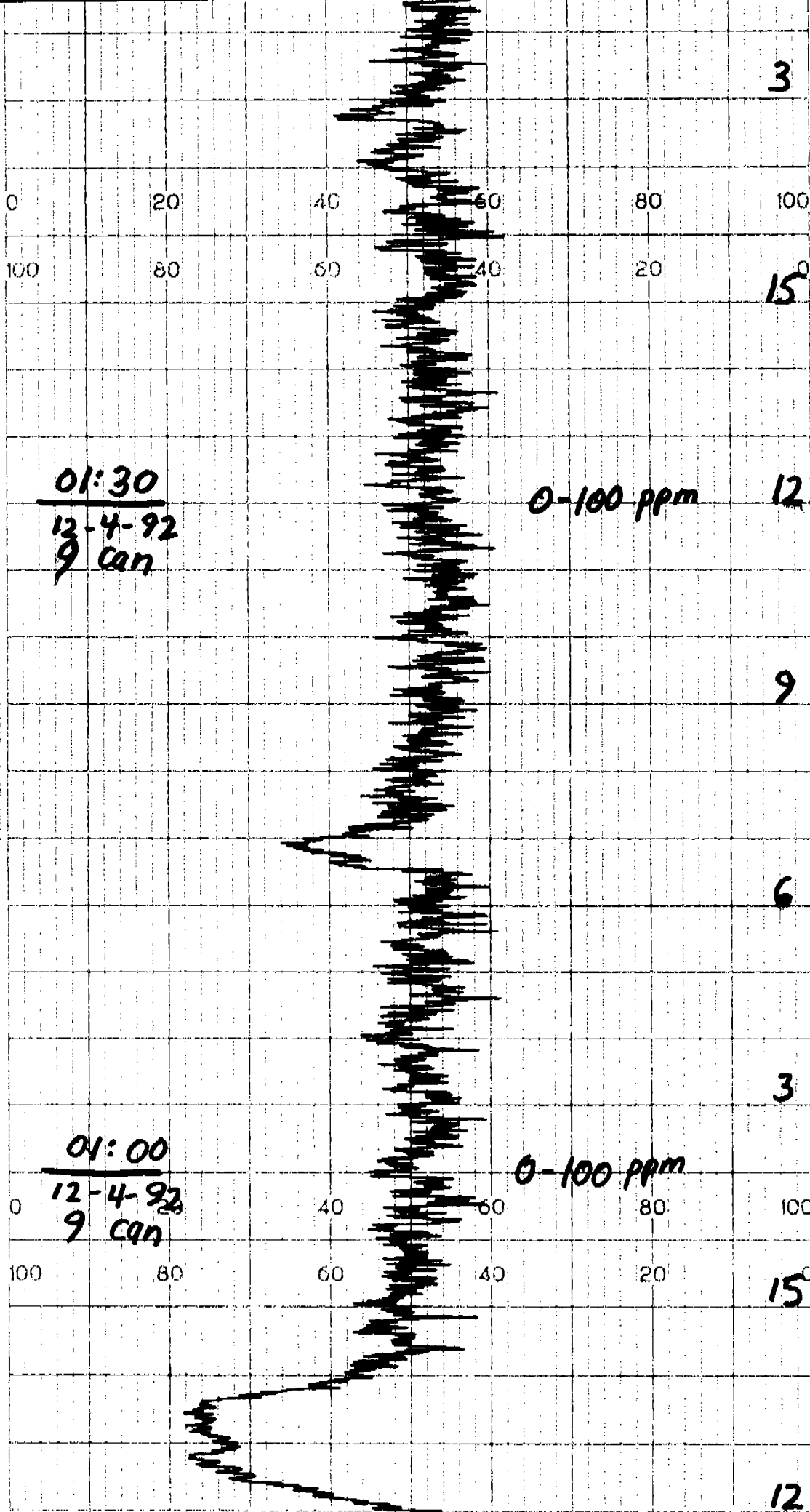


PART NO. LO/BOIS

PRINTED IN U.S.A.

PART NO. LO/BOIS

PRINTED IN U.S.A.



3

15°

12

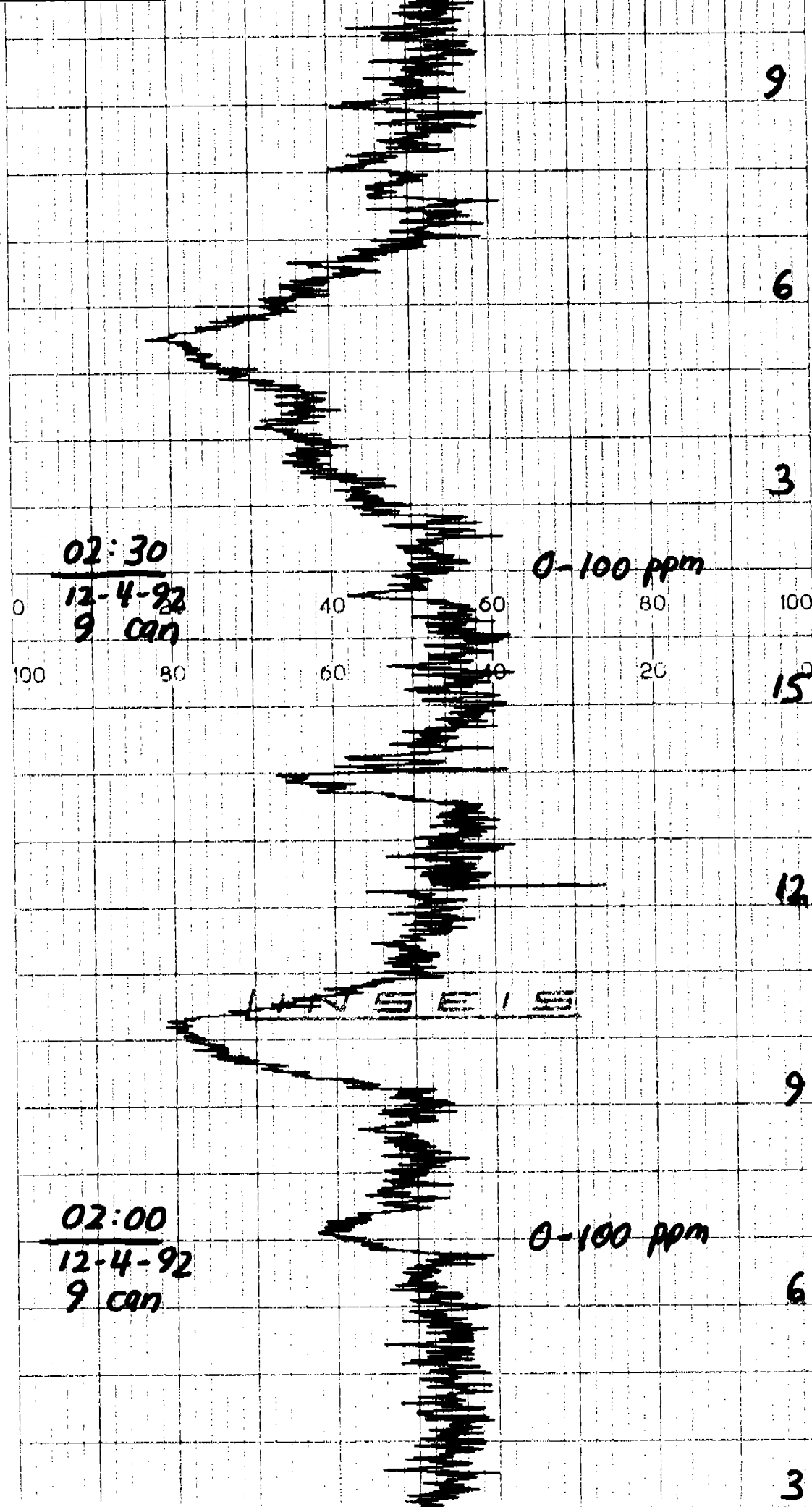
9

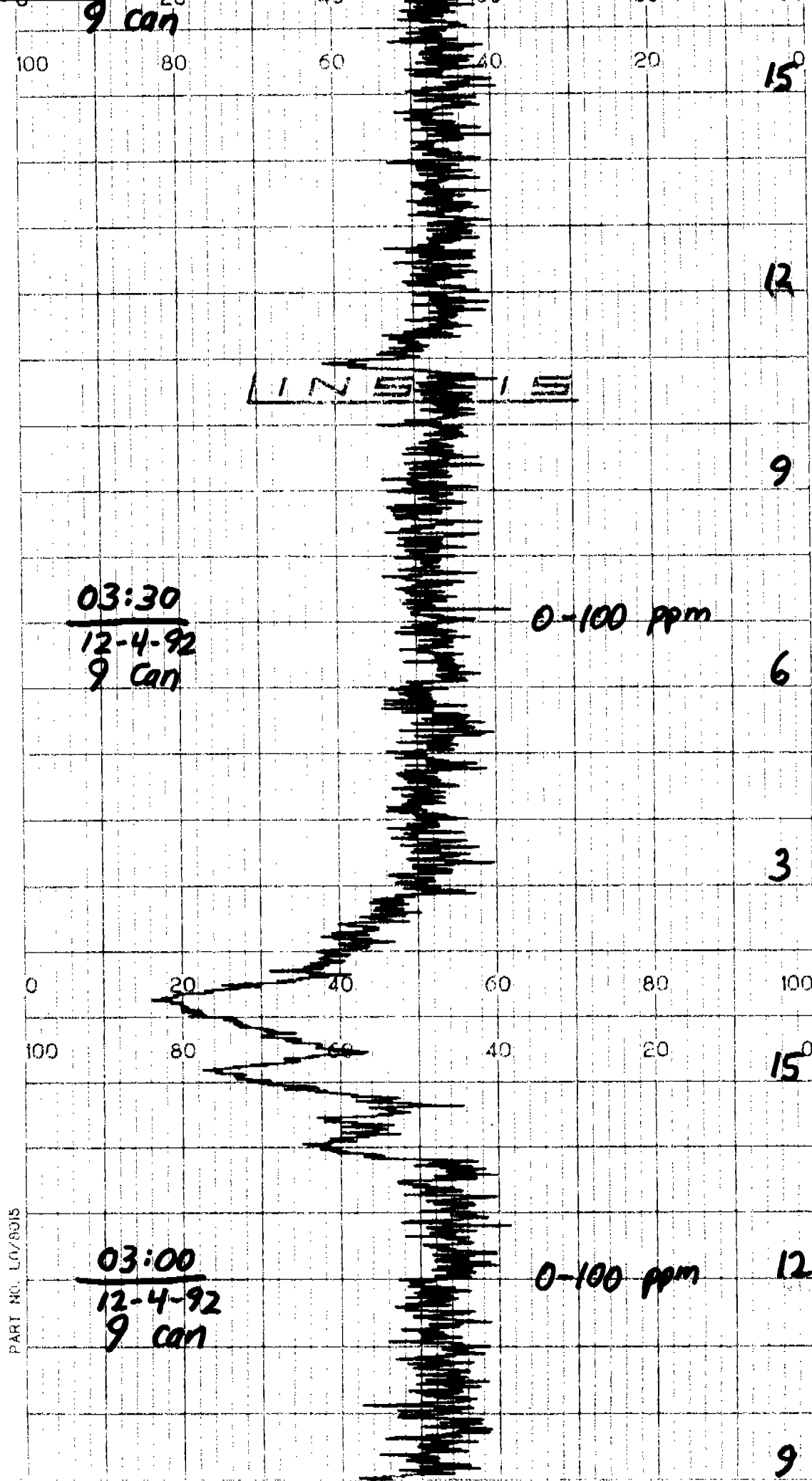
6

3

15°

12





05:00
12-4-92
9 can

0-100 ppm

6

3

0 20 40 60 80 100
100 80 60 40 20 15°

04:30
12-4-92
9 can

0-100 ppm

12

9

6

3

04:00
12-4-92
9 can

0-100 ppm

0 20 40 60 80 100
100 80 60 40 20 15°

PART NO. LD/6015

PRINTED IN U.S.A.

9 can

12

9

Scale change Full Scale = 200 ppm

05:30

6

05:30

12-4-92

9 can

0-100 ppm

3

BAG INLET #2
BAG INLET #1

START
5:27

0 20 40 60 80 100

40.1

100 ZERO

80

50.1 CALIBRATE 5:23

12-4-92

100% 9 can fill

15

12

LINE 15

9

05:00

12-4-92

9 can

0-100 ppm

6

07:00

0-200 ppm

12-4-92

9 can

3

0 20 40 60 80 100
100 80 60 40 20 15°

4

LINE IS

06:30

0-200 ppm

12-4-92

9 can

9

6

3

0 20 40 60 80 100
100 80 60 40 20 15°

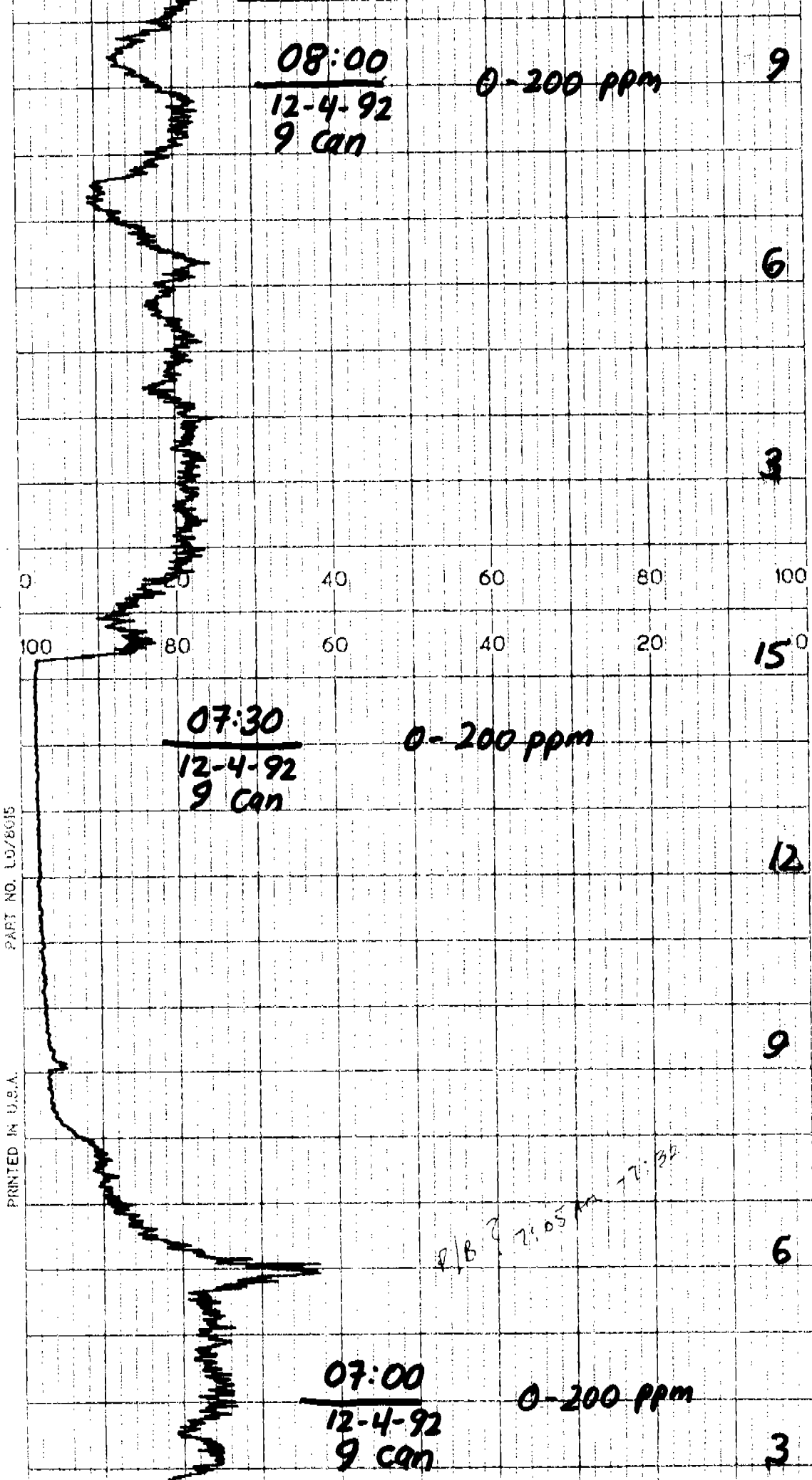
06:00

0-200 ppm

12-4-92

9 can

12



PART NO. LC78015

PRINTED IN U.S.A.

100

60

40

20

15°

09:00

12-4-92

9 can

0-200 ppm

8:56 AEW

12

9

N₂ Test

0842

6

08:30

12-4-92

9 can

0-200 ppm

3

0832

0825

12-4-92

N-Test

0

20

40

60

80

100

100

80

60

40

20

15°

12

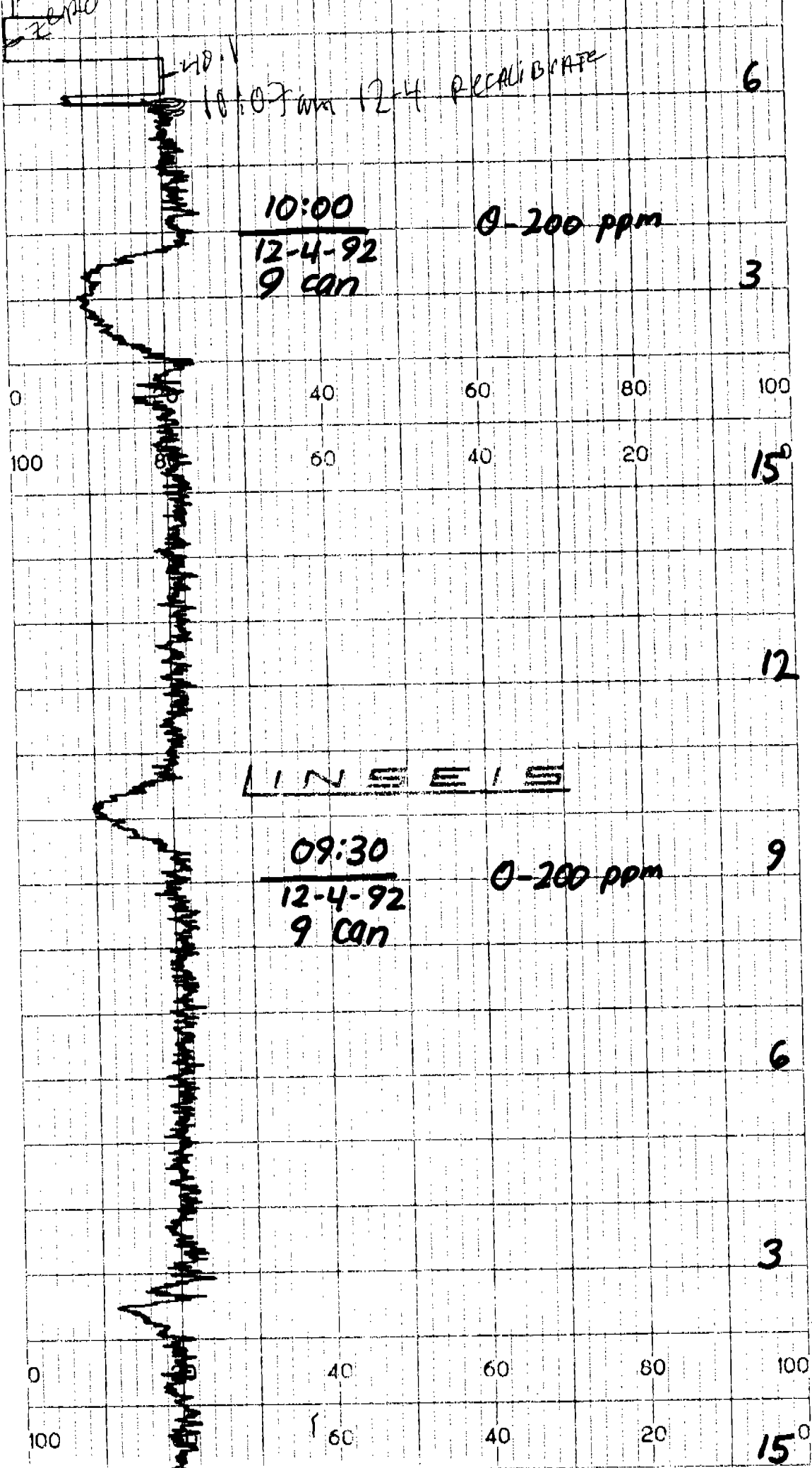
LINEIS

08:00

12-4-92

0-200 ppm

9



Intake
4 FT OFF ground at
inside door to Filter 12
Room

15E15

9

#2
BAG Inlet
#1
11:00 12-4-92

11:00
12-4-92
9 can

0-100 ppm

6

3

0 20 40 60 80 100
100 80 60 40 20 15°

PART NO. LO/8015

10:30
12-4-92
9 can

0-100 ppm

12

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- BAG Inlet #2
- BAG Inlet #1
- ZERO

10:18 Short 0-10V (0-100 ppm)

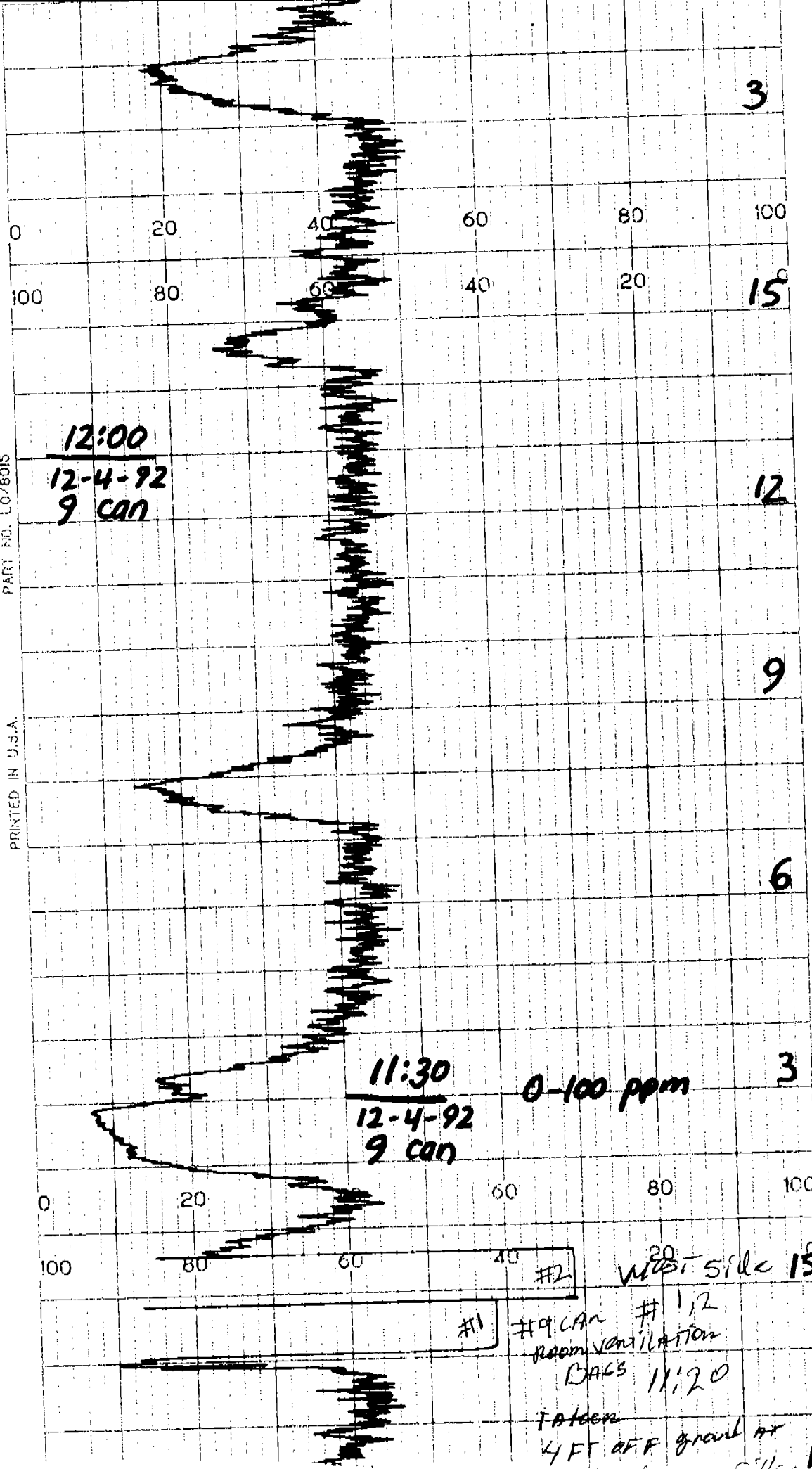
9

10:07 am 12-4 PRECALIBRATE

6

PART NO. LO/8015

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12:00
12-4-92
9 can

11:30
12-4-92
9 can

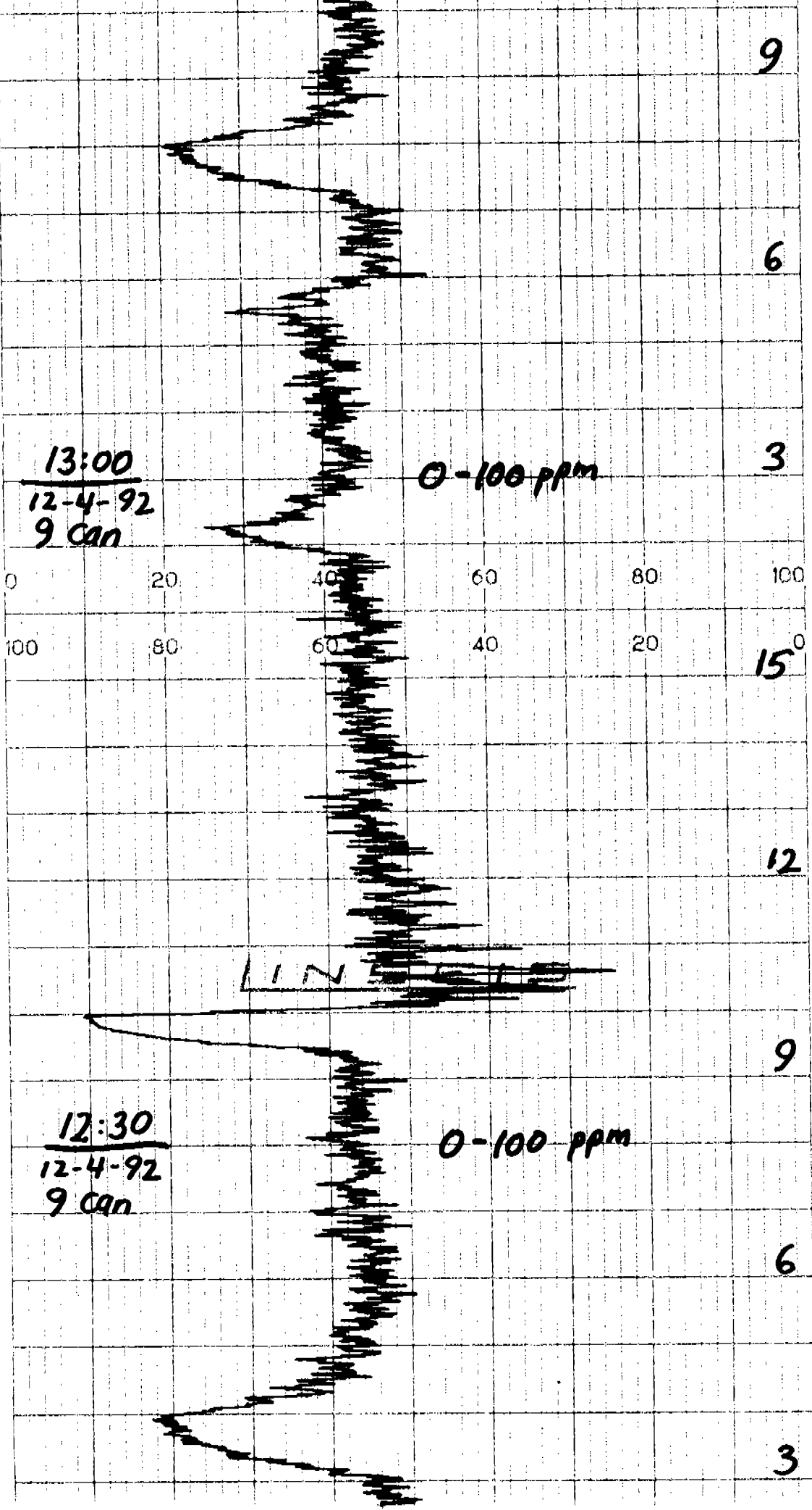
0-100 ppm

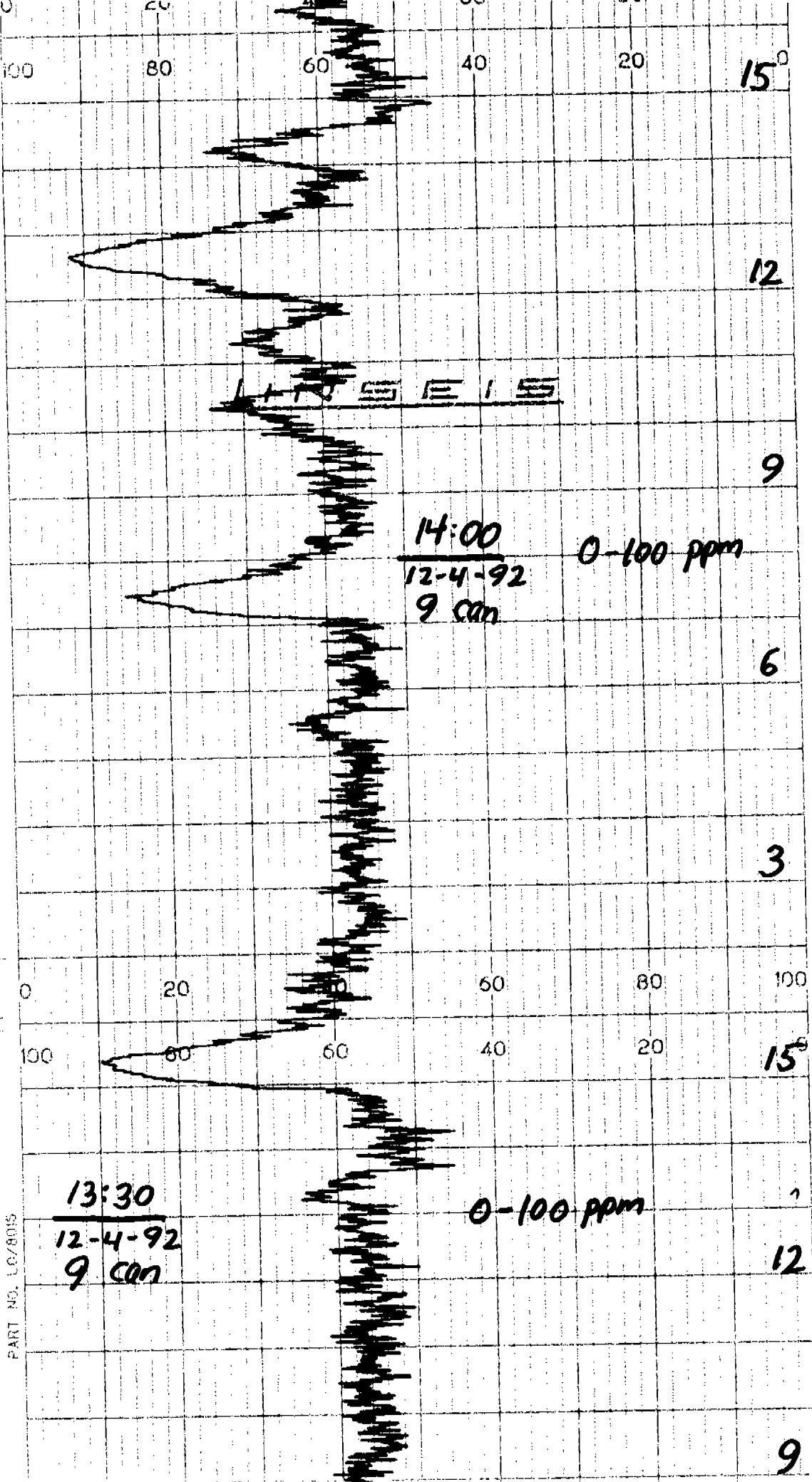
#1
#2

WAST side

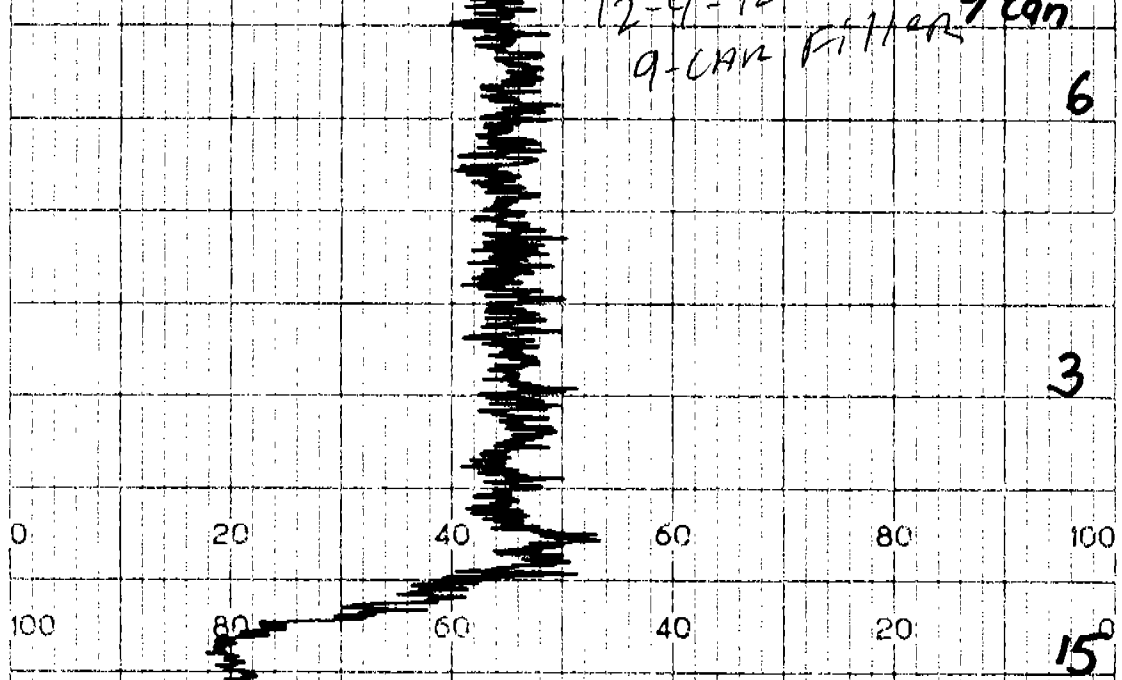
#1, 2
room ventilation
BAGS

11:20
taken
4 FT OFF ground





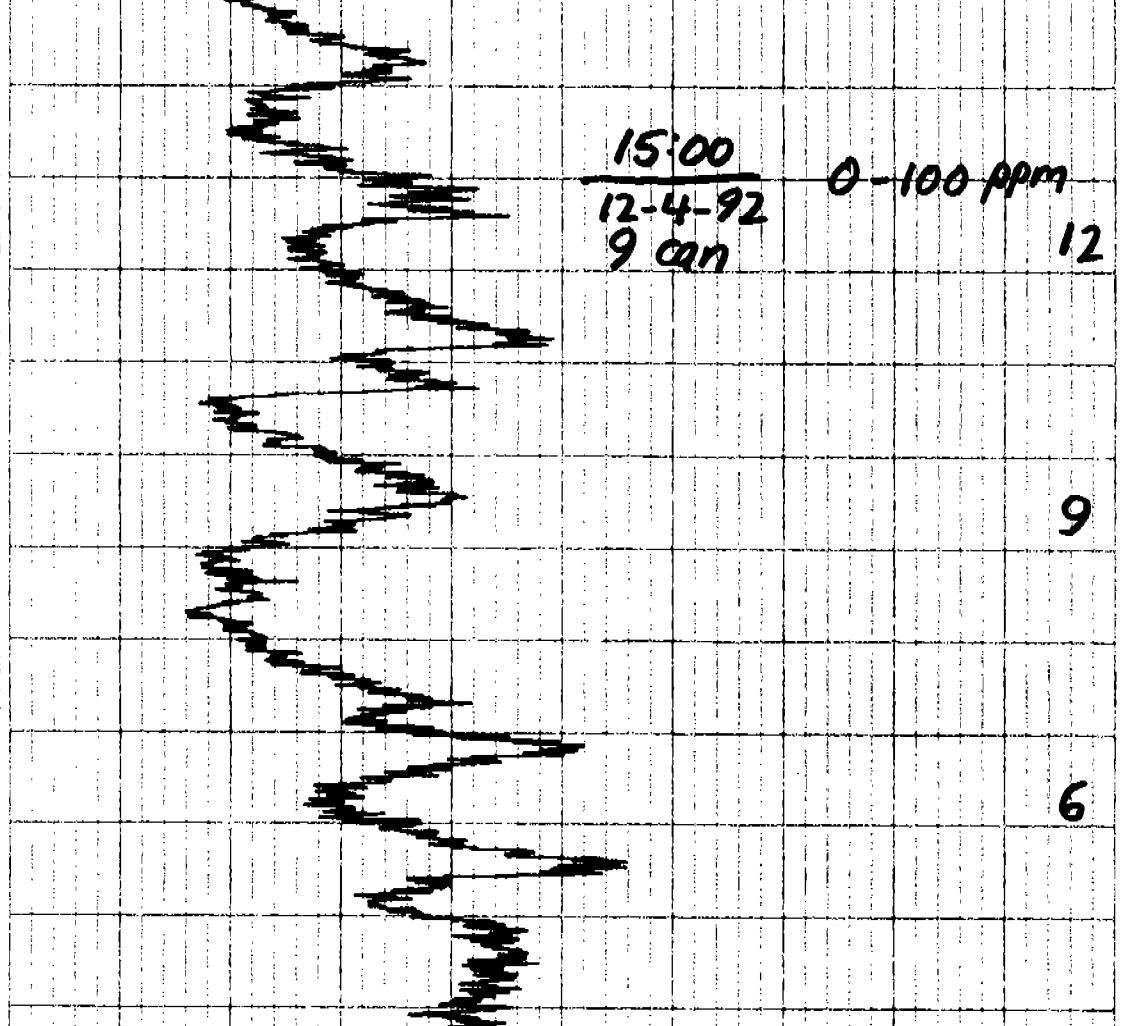
12-4-92 9-CAN FILTER 7 CAN 6



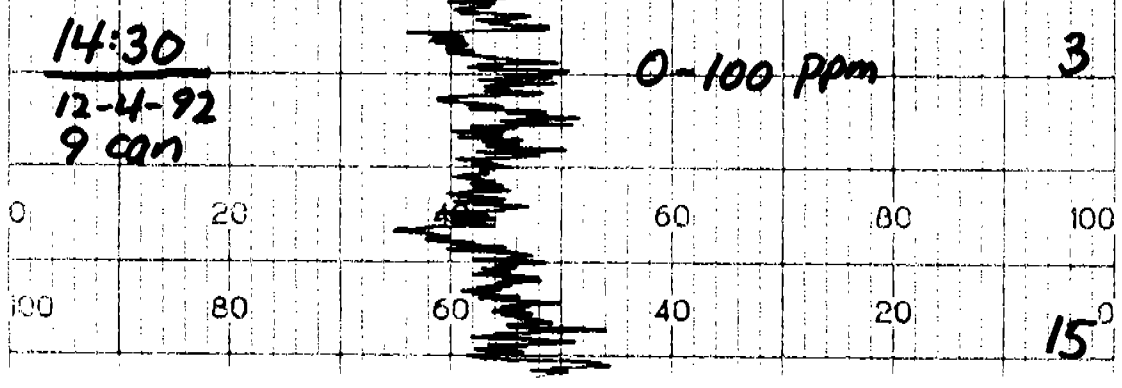
PART NO. LO/BOIS

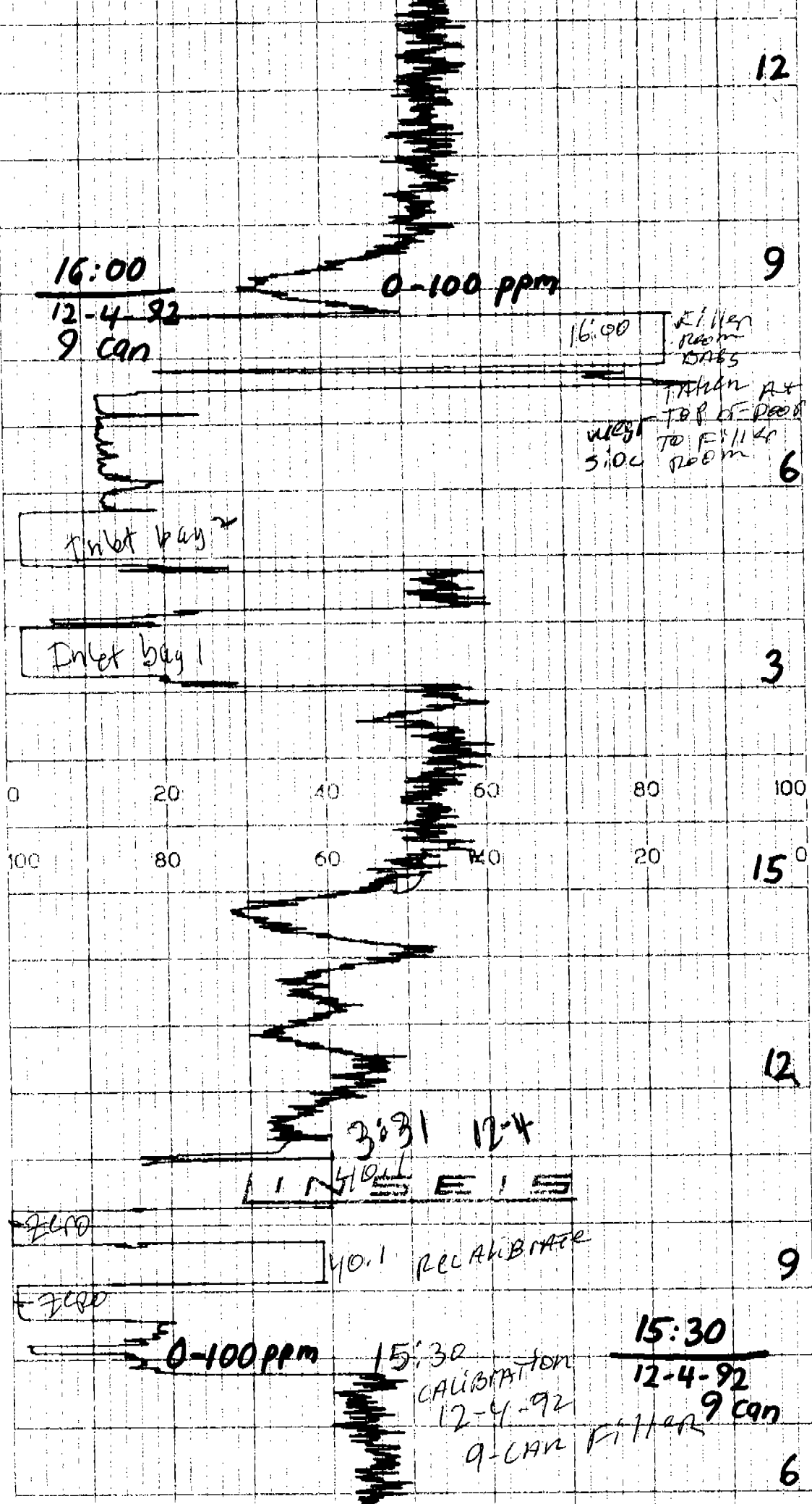
PRINTED IN U.S.A.

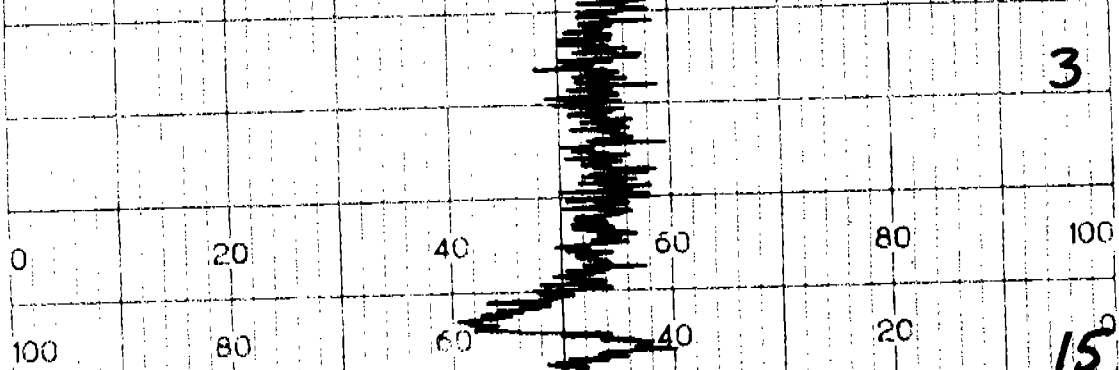
15:00
12-4-92
9 CAN 0-100 ppm 12



14:30
12-4-92
9 CAN 0-100 ppm 3







17:00
12-4-92
9 can

0-100 ppm

12

LINES 15

9

6

3

16:30
12-4-92
9 can

0-100 ppm

100

100

80

60

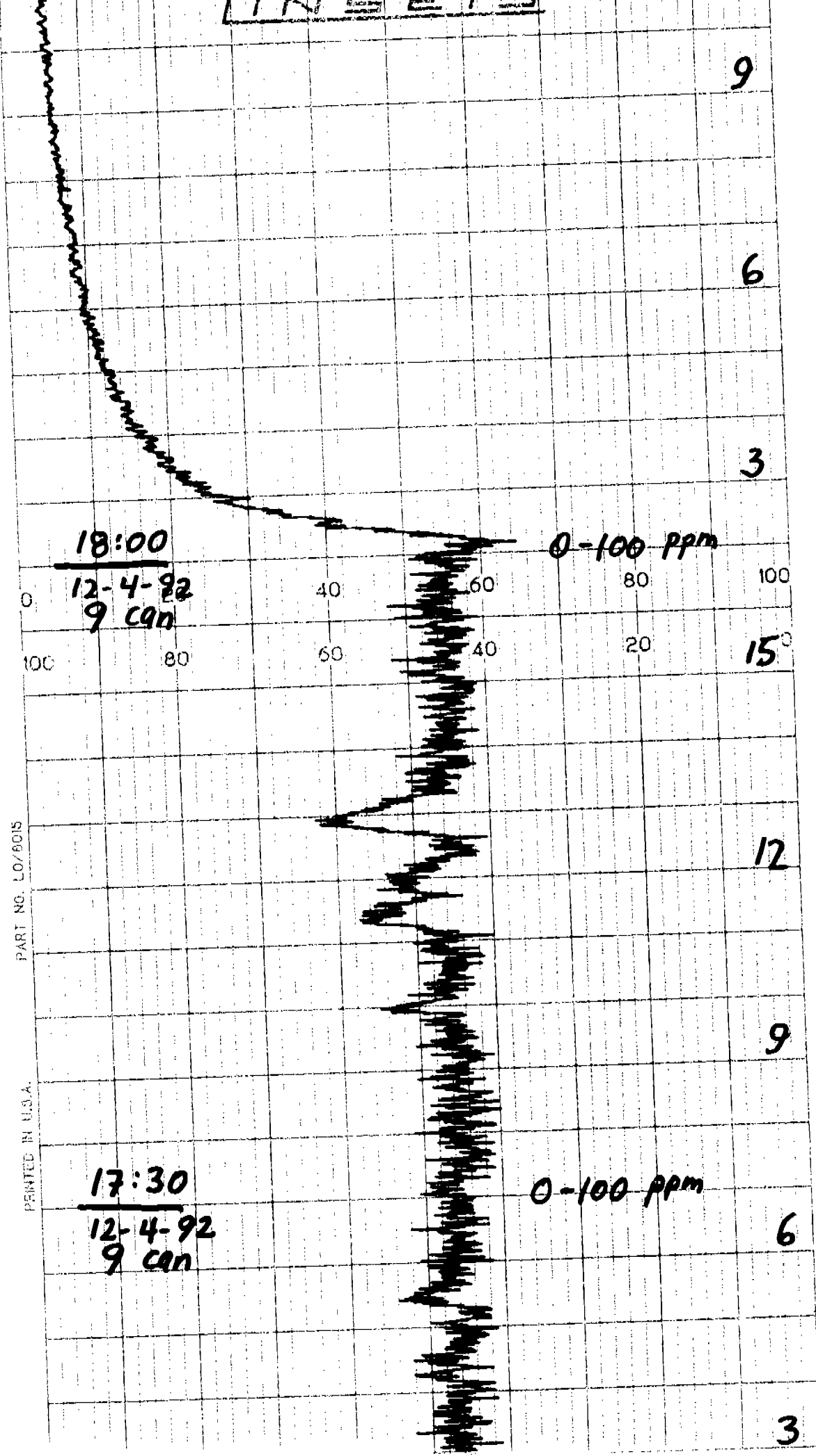
40

CHANGE H₂Orogen
16:24

15°

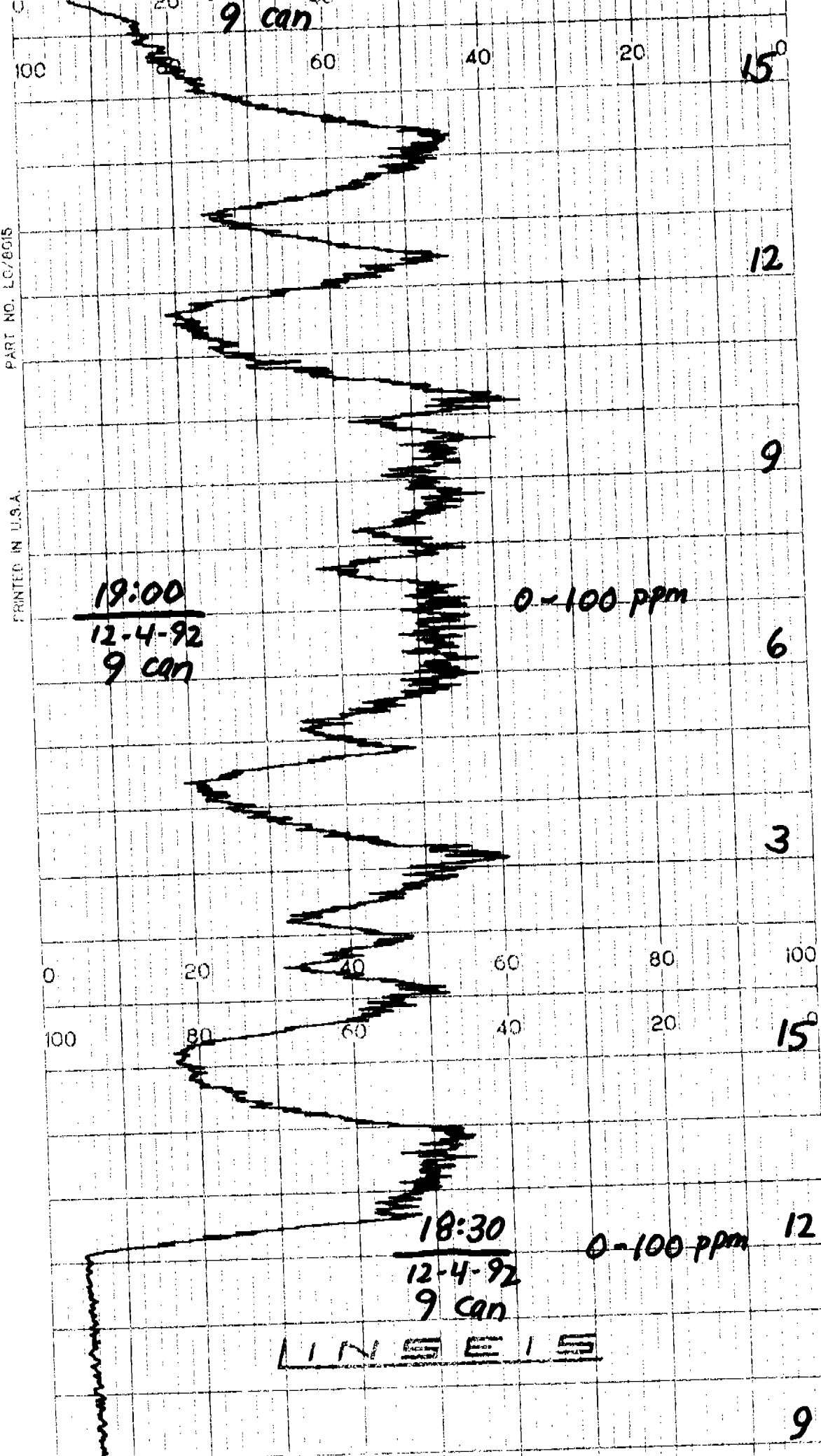
10/20/95

12



PART NO. LC/8015

PRINTED IN U.S.A.



PRIN

20:30

12-4-92
9 can

0-100 ppm

6

3

0 20 40 60 80 100
100 80 60 40 20

15°

20:00

12-4-92
9 can

0-100 ppm

12

LINE 15

9

6

3

19:30

12-4-92
9 can

0-100 ppm

0 20 40 60 80 100
100 80 60 40 20

15°

21:30

12-4-92

9 can

0-100 ppm

12

LINSEIS

9

6

3

21:00

12-4-92

9 can

0-100 ppm

0 20 40 60 80 100

100 80 60 40 20

15°

12

9

20:30

12-4-92

0 can

0-100 ppm

6

PART NO. LO/8015

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PART NO. LD/8015

PRINTED IN U.S.A.

22:30

12-4-92

9 can

0-100 ppm

3

15°

12

9

22:00

12-4-92

9 can

0-100 ppm

6

3

15°

12

21:20

PRINTED IN U.S.A.

23:30
12-4-92
9 can

0-100 ppm

9

6

3

0 20 40 60 80 100

100
23:00
12-4-92
9 can

0-100 ppm

11:01

15°C

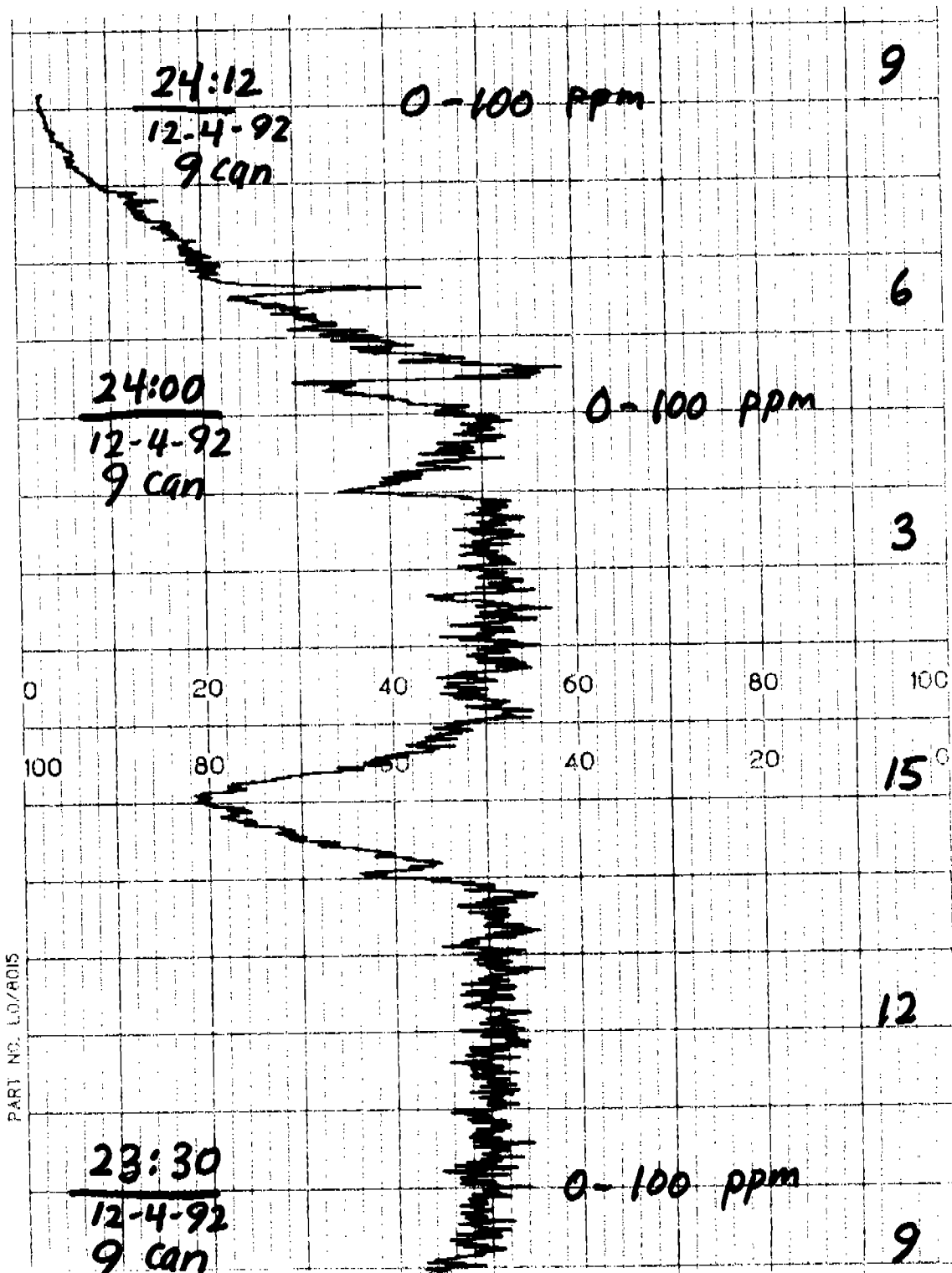
12

INSEIS

9

6

3



Appendix 4
Ethanol / Propane Conversion

Ethanol / Propane Conversion

An empirical constant for conversion of propane calibrated FIA data to true ethanol values was experimentally determined. Tedlar gas bags were filled with known volumes of hydrocarbon-free air using an SKC personal sampling pump and an NIST traceable bubble flow calibrator. The bags were then injected with precisely known masses of reagent grade ethanol, using a syringe that was weighed on a certified 0.1 mg scale before and after injection. The bags were allowed time to mix thoroughly and were analyzed using the FIA used for all filler room data collection presented in this report. Immediately before and after each bag was analyzed, the analyzer was challenged with hydrocarbon-free air and calibration gas prepared and certified in accordance with EPA Protocol 1.

Coors Brewing Company

Ethanol / Propane Conversion

Strip Chart Data

run #1	zero %FS	span %FS	span ppm	run #2	zero %FS	span %FS	span ppm
start	0.0	69.8	701	start	0.0	70.0	701
stop	0.2	69.0		stop	0.2	69.5	
	bag %FS	bag ppm			bag %FS	bag ppm	
	20.0	201.4			24.0	240.5	
run #3	zero %FS	span %FS	span ppm	run #4	zero %FS	span %FS	span ppm
start	0.0	69.5	701	start	0.0	68.0	701
stop	0.2	68.0		stop	0.0	67.5	
	bag %FS	bag ppm			bag %FS	bag ppm	
	68.0	693.3			21.3	220.4	
run #5	zero %FS	span %FS	span ppm				
start	0.0	69.5	701				
stop	0.0	69.5					
	bag %FS	bag ppm					
	30.0	302.6					

Table A4:1
Ethanol Propane Conversion
Strip Chart Data

Ethanol / Propane Conversion (continued)

Coors Brewing Company

Ethanol / Propane Conversion Data

1-14-93

Laboratory Data

	Run #1	Run #2	Run #3	Run #4	Run #5	Averages
baro. press. (mbar)	842	842	842	842	842	842
temp. (oF)	70	70	70	70	70	70
flow (lpm)	1.85	1.89	1.90	2.37	2.32	2.07
time (min.)	15.0	16.0	15.0	18.0	17.0	16.2
ethanol (g)	0.0204	0.0281	0.0773	0.0350	0.0461	0.0414
propane (ppm)	201.4	240.5	693.3	220.4	302.6	331.6

Calculations

	Run #1	Run #2	Run #3	Run #4	Run #5	Averages
ethanol (mg/scm)	890	1120	3275	991	1412	1538
propane (mg/scm)	369	441	1271	404	555	608
conversion factor	2.411	2.541	2.578	2.453	2.545	2.506

Table A4:2
Ethanol / Propane Conversion
Laboratory Data and Calculations

**Ethanol / Propane Conversion
Laboratory Data**

PART NO.

PRINTED IN U.S.A.

Zero

Zero

701 ppm C_3H_8

301.6 ppm C_3H_8

11:55

Run # 1

0 20 40 60 80 100
100 80 60 40 20 15°

11:45

301.6 ppm C_3H_8 11:30

701 ppm C_3H_8

Zero

LINE IS

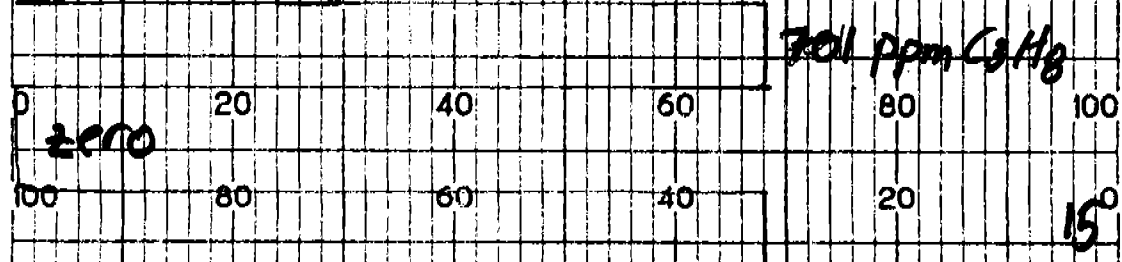
Coors Brewing Company
Ethanol / Propane Conversion

1-14-93 50 cm³/hr

STANDARD FOR COORS

PG:CB30105

10 V.



701 ppm C_3H_8

zero

Run #3

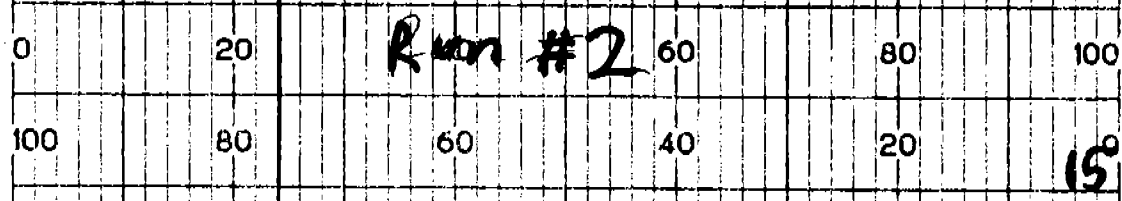
L I N E I S

13:40

zero

701 ppm C_3H_8

301.6 ppm C_3H_8



Run #2

12:55

301.6 ppm C_3H_8

701 ppm
~~701~~ C_3H_8

zero

PART NO. LG/8015

16:40

Run # 5

6

3

100

80

60

40

20

0

150

20

40

60

80

100

301.6 16:30

12

701 ppm C_3H_8

PART NO. L.O./8015

zero

701 ppm C_3H_8

301.6 ppm C_3H_8

9

zero

PRINTED IN U.S.A.

Run # 4

6

6

3

3

301.6 ppm C_3H_8

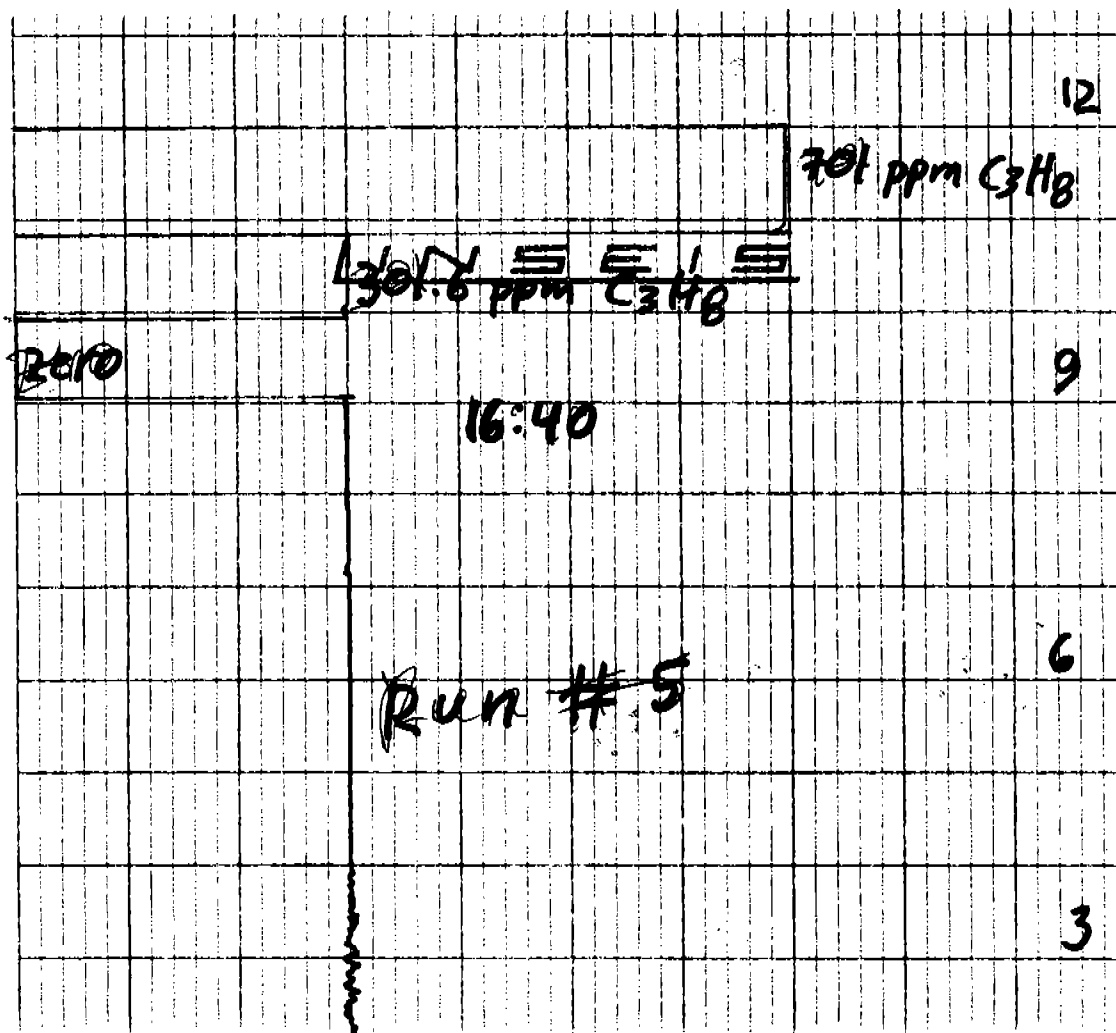
701 ppm C_3H_8

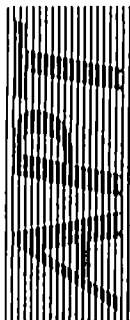
100

80

60

40





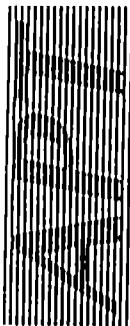
AIR POLLUTION TESTING, INC.

Client	Coors Brewing Co
	Golden, CO
Date	1-14-93

Sketch Location 1	Sketch Location 2
-------------------	-------------------

Pump # PCXR7		Pre-test flow (liter/min)	Post-test flow (liter/min)	Mid-test flow (liter/min)	Notes: Run #1
Method # Ethanol $\rightarrow$ Propane		1.88	1.85		Syringe Mass
Ta 70	Pb 842	1.82	1.86		2.0275 tare
Start time 11:25	Stop time 11:40	1.86	1.85		2.0071 final
Average Flows (liter/min)	1.85	1.85	1.85		0.0204 diff

Pump #	PCXR 7	Pre-test flow (liter/min)	Post-test flow (liter/min)	Mid-test flow (liter/min)	Notes: Run #2
Method #	Ethanol $\rightarrow$ Propane	1.89	1.90		Syringe Mass
Ta	70	Pb 842	1.89	1.88	2.0249 tare
Start time	12:34	Stop time 12:50	1.91	1.86	1.9968 final
Average Flows (liter/min)	1.89	1.90	1.88		0.0281 $\rightarrow$ diff



AIR POLLUTION TESTING, INC.

Client	Coors Brewing Co
	Golden, Co
Date	1-14-93

Sketch Location 1	Sketch Location 2

Pump #	PCXR7	Pre-test flow (liters/min)	Post-test flow (liters/min)	Mid-test flow (liters/min)	Notes: Run #3
Method #	Ethanol $\rightarrow$ Propane	1.88	1.89		Syringe Mass
Ta	70	Pb 842	1.88	1.90	2.0783 tare
Start time	13:20	Stop time 13:35	1.96	1.89	2.0010 final
Average Flow (liters/min)	1.90	1.91	1.89		0.0773 diff

Pump #	PCXR7	Pre-test flow (liters/min)	Post-test flow (liters/min)	Mid-test flow (liters/min)	Notes: Run #4
Method #	Ethanol $\rightarrow$ Propane	2.41	2.35		Syringe Mass
Ta	70	Pb 842	2.40	2.36	2.0415 tare
Start time	14:25	Stop time 14:43	2.36	2.35	2.0065 final
Average Flow (liters/min)	2.37	2.39	2.35		0.0350 diff



AIR POLLUTION TESTING, INC.

Client	Coors Brewing Co
	Golden, CO
Date	1-14-93

Sketch Location 1	Sketch Location 2
-------------------	-------------------

Pump #	PCXR7	Pre-test flow (liter/min)	Post-test flow (liter/min)	Mid-test flow (liter/min)	Notes: Run #5
Method #	Ethanol → Propane	2.34	2.33		Syringe Mass
Ta	70	Pb 842	2.31	2.30	2.0334 tare
Start time	16:08	Stop time 16:25	2.29	2.33	1.9873 final
Average Flow (liter/min)	2.32	2.31	2.32		0.0461 diff

Pump #		Pre-test flow (liter/min)	Post-test flow (liter/min)	Mid-test flow (liter/min)	Notes:
Method #					
Ta	Pb				
Start time	Stop time				
Average Flow (liter/min)					

Hydrocarbon Response Factors

6/90

Component	Resp.-Factor JUM-1	Resp.-Factor JUM-2
Methane	1.02	1.04
Propane	1.00	1.00
Acetylene	0.92	0.94
n-Butane	0.98	0.98
n-Hexane	0.85	0.86
n-Heptane	0.91	0.93
iso-Octane	0.99	0.98
cyclo-Hexane	0.93	0.94
Methanol	0.69	0.68
Ethanol	0.65	0.67
iso-Propanol	0.82	0.81
Benzene	1.05	1.05
Toluene	1.02	1.03
4-Ethyltoluene	0.88	0.89
p-Xylene	0.91	0.90
Acetone	0.72	0.73
Diethylether	0.75	0.77
Acetic Acid	0.58	0.55
Acetic Acid Ethylester	0.70	0.72
Acetic Acid Isobutylester	0.88	0.89
Dichloromethane	1.09	1.06
Chloroform	0.82	0.78
1, 1, 1-Trichlorethane	1.06	1.02
Trichlorethane	1.03	1.01
Tetrachlorethane	1.22	1.20
Chlorobenzene	1.01	1.04
Number of Compounds	26	26
Average	0.903	0.903
Standard Tolerance	0.154	0.152

Data Compiled By :Tuv
 Analyzer Type :Model VE-7
 Fuel Type :100% H₂
 Calibration Gas :Propane

Note: The response factors are calculated as mg (carbon) per m³.

Appendix 5
Production Data

M E M O R A N D U M

DECEMBER 08, 1992

TO: TOM BUEB

FROM: MIKE MURPHY

SUBJECT: BARRELAGES DURING PACKAGING STACK TESTING

The following is a listing of the number of cases/barrels produced during the air emissions stack testing on December 2, 3 and 4, 1992:

3 BOTTLE FILLER ROOM VENT

Total cs/bbls.

9 a.m. - 1 p.m. - 4700 cs. (12 oz.) => 341 bbls.

NOTE: The testing consisted of three one hour runs, with calibration time (approx. 10 min.) in between. Since these tests did not start exactly on the hour or half hour, it is very difficult to estimate the exact number of cases/barrels produced during the actual test runs.

5F/1CAN FILLER ROOM VENT

Total cs/bbls.

5 p.m. - 8:15 p.m. - 9300 cs. (12 oz.) => 675 bbls.

NOTE: The testing consisted of three one hour runs, with calibration time (approx. 10 min.) in between. Since these tests did not start exactly on the hour or half hour, it is very difficult to estimate the exact number of cases/barrels produced during the actual test runs.

9-1 FILLER ROOM VENT

Total cs/bbls.

7 a.m. Thursday (12/3) -

11:59 p.m. Friday (12/4) - 69934 cs. (12 oz.) => 5076 bbls.

Considerations:

- 7 a.m. - 3 p.m. (12/3) Sterilization of this filler.
- 7 a.m. - 7:20 a.m. (12/4) Pushback from Repeal Coors to 3.2 Coors beer.
- 8:20 a.m. - 8:55 a.m. (12/4) Nitrogen test conducted.

Conversion factors for cases to barrels are:

12 oz. (cans or btls.) - (# cs. * .07258)

#3-1 BOTTLE FILLER ROOM

DATE AND TIME	ROOM STATIC + "WC	ROOM LEAKAGE IN FPM	ROOM TEMP IN F	ROOM HUMID- ITY % RH	ROOF WIND DIRECT- ION	ROOF WIND SPEED IN MPH	ROOF AIR TEMP IN F	NOTE
12/2/92 9:30 AM	0.02	870	69	33	WEST	2.4	28	*1
12/2/92 10:00 AM	0.02	850	68	36	--	--	--	*2
12/2/92 10:30 AM	0.02	840	67	35	SE	6.2	28	*3
12/2/92 11:00 AM	0.02	860	67	42	--	--	--	*4
12/2/92 11:30 AM	0.02	880	66	38	SE	3.9	30	*4
12/2/92 12:NOON	0.018	860	66	38	--	--	--	*4
12/2/92 12:30 PM	0.018	830	67	35	SE	3.7	31	*4
12/2/92 1:00 PM	0.018	850	65	37	--	--	--	*5

- *1. START RUNNING 9:00AM, #3-2 FILLER DOWN.
- *2. #3-1 RUNNING, #3-2 DOWN.
- *3. #3-1 DOWN, CAPPER PROBLEM, 5-10 MIN.
- *4. #3-1 RUNNING, #3-2 DOWN.
- *5. END OF TEST.

FILRMTST

#5 CAN FILLER ROOM

DATE AND TIME	ROOM STATIC + "WC	ROOM LEAKAGE IN FPM	ROOM TEMP IN F	ROOM HUMID- ITY % RH	ROOF WIND DIRECT- ION	ROOF WIND SPEED IN MPH	ROOF AIR TEMP IN F	NOTE
---------------------	-------------------------	---------------------------	----------------------	-------------------------------	--------------------------------	---------------------------------	-----------------------------	------

12/2/92 5:10 PM	0.006	340	72	33	ESE	3.9	28	
--------------------	-------	-----	----	----	-----	-----	----	--

12/2/92 5:30 PM	0,01	350	72	33	ESE	3.4	26	*1
--------------------	------	-----	----	----	-----	-----	----	----

12/2/92 5:50 PM	0.005	330	72	33	WEST	4.3	25	*2
--------------------	-------	-----	----	----	------	-----	----	----

*1. SEAMER DOWN TWO MINUTES DURING ROOM TEST.

*2. FILLER DOWN TWO MINUTES DURING ROOM TEST.

#9-1 CAN FILLER ROOM

DATE AND TIME	ROOM STATIC + " WC	ROOM LEAKAGE IN FPM	ROOM TEMP IN F	ROOM HUMID- ITY % RH	ROOF WIND DIRECT- ION	ROOF WIND SPEED IN MPH	ROOF AIR TEMP IN F	NOTE
12/3/92 9:45 AM	0.01	1140	73	20	SW	3.4	24	*1
12/3/92 2:15 PM	0.08	1130	78	17	SE	2.5	21	*2
12/3/92 3:50 PM	0.09	1290	72	27	SE	6.2	21	*3
12/4/92 8:30 AM	0.085	1300	69	24	CALM	0.0	20	*4
12/4/92 1:00 PM	0.09	1320	69	24	CALM	0.0	20	*5

- *1. FILLER DOWN, NO PRODUCTION.
- *2. FILLER DOWN, NO PRODUCTION, SNOW FALLING.
- *3. PRODUCTION STARTED RUNNING 3:15 PM.
- *4. FILLER RUNNING, SNOW FALLING.
- *5. FILLER DOWN ONE MIN DURING ROOM TEST.

FILLER ROOM CO2 CONCENTRATION AND POSITIVE PRESSURE DATA:

PHIL BARKER 12-7-92

DATE	TIME	%CO2	ROOM PRESSURE
#3 BOTTLE LINE			
12/2/92	9:30 AM	.55	.02 IN. OF H2O
	10:00	.50	.02
	10:30	.55	.018
	11:00	.65	.019
	11:30	.70	.017
	12:00	.80	.018
	12:30 PM	.80	.018
	1:00	.90	.018
#5 CAN LINE			
12/2/92	5:30 PM	.15	.01
	6:30	.15	.01
	7:30	.15	.00
	8:30	.15	.00
#9 CAN LINE			
12/4/92	11:30 AM	.01***	***
	4:00 PM	.02	.02
12/5/92	7:30 AM	.02	.018
	3:00 PM	.18	.018

*** READING TAKEN PRIOR TO START-UP

1/4
Filler Room VOC Test's

Ed Hudson's Notes
&
Observations.

3 Bottle (12/2/92)

9 AM - start of run, intermittent operation
at first. - Keystone light

9:20 AM - Consistent and steady filling operation

9:57 - intermittent operation.

11 AM - 2nd hour of VOC monitoring
on exhaust duct started.

Overall preliminary results from ATP

Inlet 6000 dscfm
Outlet 1500 dscfm

Inlet VOC = 2-3 ppm

Outlet VOC = 30 ppm

Filler #5

(12/2/92)

5 PM - started sampling
Ambient Air in basement = 30ppm CO₂
Continuous sampling of exhaust
for 3 1 hr samples.

Pull bag samples on shroud air supply
for VOC levels.

Holes for velocity transverse measurements
not cut, will have to get velocity profiles
at later date.

5:45 - filler idle, table full
5:47 - " " " "
5:49 - " " " " , operator
using pop gun.

5:51 - filler stopped by operator

5:52 - Running

Outlet air velocity = 3900 acfm
= 3105 dscfm

7:30 - Noticed static pressure gauge went
to a negative peg.

8:15 - End of exhaust monitoring
Ambient air CO₂ = 16ppm

8:24 - static pressure gauge again
pegged negative

9 Filler

12/3/92

3:15 PM ~~started~~ Filler started

12/4/92

6:21 AM - beer spill in filler room - bent can

~~before~~ before shot down $CO_2 = 0.05 - 0.1\%$
pushback

7:06 AM - ~~beer out~~ Finished Filling
beer dumped on floor

7:08 AM - CO_2 peaked at 0.7%
at operator head level

7:11 AM - $CO_2 = 0.2\%$

7:13 AM - started Wash down
 $CO_2 = 0.1\%$

7:17 AM - ~~start~~ Finished Wash down
 $CO_2 = 0.1\%$

7:35 AM - started Filling

7:43 AM - $CO_2 = 0.18$
static Pressure = 0.9" H₂O

7:51 Wash down

9 Filler
(continued)

8:21A - steam in closure off
N₂ on

8:23A - Positive N₂ flow - didn't
have N₂ before this time

8:48A - N₂ off
steam ON

Time back to Tom Bueb's
watch from which times
around N₂ Test were written
on strip chart.

Tom B Time + 30 seconds = time
of my observations.

**Coors Brewing Company
#6 Can Filler Room
Production Data**

12-22-92

Verbal from Mike Murphy, Coors Brewing Company:

Beer filling on 12-16-92 for period of VOC testing was 650 bbls.

Relayed to:

A handwritten signature in black ink, appearing to read "Paul Ottenstein", with a long horizontal flourish extending to the right.

Paul Ottenstein
Project Manager

Appendix 6
Calibration Certificates



Shipped from:
Scott Specialty Gases
Route 611
Plumsteadville, PA 18949
Purchase order :
91047

Shipped to:
AIR POLLUTION TESTING INC
ATTN: POW91047
4535 W 68TH AVE
WESTMINSTER, CO 80030

Project No 0134629

Certified per E.P.A. Protocol # 1 Procedure WG1 Section # 3.0.4
 Certified accuracy +/- 1 X NIST Traceable

Cylinder number	ALM002673	Cylinder pressure	Date of assay:	1/23/92
		2000 psig.		
Component		Certified concentration	Expiration date:	7/23/93
PROPANE		12.24 ppm		
NITROGEN		Balance		

Standard	
Type	GMIS
Concentration	14.99 ppm
Cylinder #	AAL-12327

```
Analyzer
Make      : VARIAN
Model     : VA3300
Serial number : 7945
Analytical principle : FID
Date of calibration : 1/23/92
```

Raw data units:	AREA	Concentration	of Customer	Cylinder
Analysis	1/23/92			
Z1=0.00	R1=67168	T1=54766	12.22	ppm
R2=67173	Z2=0.00	T2=54787	12.23	ppm
Z3=0.00	T3=54905	R3=67021	12.28	ppm

Analyst

Approved by

Mark S. Sirinides/Ted Neeme



Shipped from:
Scott Specialty Gases
Route 611
Plumsteadville, PA 18949
Purchase order :
91047

Shipped to:
AIR POLLUTION TESTING INC
ATTN: POW91047
4535 W 68TH AVE
WESTMINSTER, CO 80030

Project No 0134629

Certified per E.P.A. Protocol # 1 Procedure #G1 Section # 3.0.4
 Certified accuracy +/- 1 X NIST Traceable

Cylinder number	ALM016822	Cylinder pressure	Date of assay:	1/23/92
		2000 psig.		
Component		Certified concentration	Expiration date:	7/23/93
PROPANE		40.1 ppm		
NITROGEN		Balance		

Standard	
Type	GMIS
Concentration	98.21 ppm
Cylinder #	CAL4282

```
Analyzer
Make      : VARIAN
Model     : VA3300
Serial number : 7945
Analytical principle : FID
Date of calibration : 1/23/92
```

[illegible]

Analyst

Approved by

Mark S. Sirinides/Ted Neeme



Scott Specialty Gases, Inc.

E. P. A. PROTOCOL CERTIFICATE OF ANALYSIS

Shipped from:
Scott Specialty Gases
Route 611
Plumsteadville, PA 18949
Purchase order :
91047

Shipped to:
AIR POLLUTION TESTING INC
ATTN: POW91047
4535 W 68TH AVE
WESTMINSTER, CO 80030

Project No 0134629

Certified per E.P.A. Protocol # 1 Procedure #G1 Section # 3.0.4
Certified accuracy +/- 1 % NIST Traceable

Cylinder number	ALM019712	Cylinder pressure	Date of assay:	1/23/92
		2000 psig.		
Component		Certified concentration	Expiration date:	7/23/93
PROPANE		91.3 ppm		
NITROGEN		Balance		

Standard
Type
Concentration
Cylinder #

GMIS
98.21 ppm
CAL4282

Analyzer
Make : VARIAN
Model : VA3300
Serial number : 7945
Analytical principle : FID
Date of calibration : 1/23/92

Raw data units:	AREA	:	:	Concentration	:
		:	:	of Customer	:
		:	:	Cylinder	:
Analysis	1/23/92	:	:		:
		:	:		:
Z1=0.00	R1=432474	T1=402119	:	91.3	ppm
R2=432431	Z2=0.00	T2=402018	:	91.3	ppm
Z3=0.00	T3=402149	R3=432116	:	91.4	ppm
			:		
			:		
			:		
			:		
			:		
			:		
			:		
			:		

Analyst

Paul White

Approved by

Mark S. Sirinides

Mark S. Sirinides/Ted Neeme

Scott Specialty Gases

500 WEAVER PARK ROAD, LONGMONT, COLORADO 80501 (303) 442-4700 Fax (303) 772-7673

Shipped From : Scott Colorado
 Date Shipped : 8-18-92
 Our Project # : 808272
 Your P.O. # : 92-693
 Page of
 Expiration Date : 02/07/94

Customer : AIR POLLUTION TESTING INC
 4535 W. 68TH AVE
 WESTMINSTER CO 80030

**** CERTIFICATE OF ANALYSIS - EPA PROTOCOL GASES ****

Certified Per Traceability Protocol # 1 Section 3.0.4

Certified Accuracy 1 % NIST Traceable File # APT301C3

Cylinder Number AAL-6506
 Cylinder Pressure 2000 psig
 CGA Fitting 350
 QC Number 22139217

REFERENCE STANDARDS GAS ANALYZER

COMPONENT	CERTIFIED CONC.	SRM # (CRM #)	CYLINDER NUMBER	CONC.	MAKE/MODEL	LAST CALIBRATION DATE	ANALYTICAL PRINCIPLE
PROPANE	301.6 PPM	2646 GMS*	AAL-18342 1L-14382	973.0 PPM 314.0 PPM	HEWLETT-PACKARD/5890A 3115A34623	07-13-92	FLAME IONIZATION

BALANCE GAS : NITROGEN

FIRST ANALYSIS

ZERO GAS (mV)	TEST GAS (mV)	RESULTS PPM
0.00	0.3020	302.0
0.00	0.3020	302.0
0.00	0.3020	302.0

CALCULATED RESULTS
 302.0
 302.0
 302.0

AVERAGE : 302.0 PPM

DATE : 07/31/92

REFERENCE GAS CONC.	ZERO GAS (mV)	TEST GAS (mV)	RESULTS PPM
314.0 PPM	0.3140	0.3011	301.1
0.3140	0.3140	0.3011	301.1
0.3140	0.3140	0.3011	301.1

CALCULATED RESULTS
 301.1
 301.1
 301.1

AVERAGE : 301.1 PPM

DATE : 08/07/92

REFERENCE GAS CONC.	TEST GAS (mV)	RESULTS PPM
314.0 PPM	0.3140	314.0
0.3140	0.3140	314.0
0.3140	0.3140	314.0

SRM # (CRM #)	CONC. %	SPLIT PT (%)	DVM (mV)	FITTED VALUE	PERCENT ERROR
0.00	0	0	0.00	0.00	0.00
0.00	0	0	0.00	0.00	0.00
0.00	0	0	0.00	0.00	0.00
0.00	0	0	0.00	0.00	0.00
0.00	0	0	0.00	0.00	0.00
0.00	0	0	0.00	0.00	0.00

* GMS - GAS MANUFACTURER'S INTERNAL STANDARD

Analyst : David Chapman

Approved By :

RIC SCHMELTEKOPF



Scott Specialty Gases, Inc.

E. P. A. PROTOCOL CERTIFICATE OF ANALYSIS

Shipped from:
Scott Specialty Gases
Route 611
Plumsteadville, PA 18949
Purchase order :
91047

Shipped to:
AIR POLLUTION TESTING INC
ATTN: POW91047
4535 W 68TH AVE
WESTMINSTER, CO 80030

Project No 0134629

Certified per E.P.A. Protocol # 1 Procedure #G1 Section # 3.0.4
Certified accuracy +/- 1 % NIST Traceable

Cylinder number	ALM016808	Cylinder pressure	Date of assay:	1/20/92
		2000 psig.		
Component		Certified concentration	Expiration date:	7/20/93
PROPANE		701 ppm		
NITROGEN		Balance		

Standard
Type
Concentration
Cylinder #

GMIS
750.4 ppm
A-012415

Analyzer
Make : VARIAN
Model : VA3300
Serial number : 7945
Analytical principle : FID
Date of calibration : 11/11/91

Raw data units:	AREA	:	:	Concentration	:
		:	:	of Customer	:
		:	:	Cylinder	:
Analysis	1/20/92	:	:		:
		:	:		:
Z1=0.00	R1=60210	T1=56314	:	: 702	ppm
R2=60103	Z2=0.00	T2=56091	:	: 700	ppm
Z3=0.00	T3=56017	R3=60025	:	: 700	ppm
			:	:	:
			:	:	:
			:	:	:
			:	:	:
			:	:	:
			:	:	:
			:	:	:

Analyst

Paul Neeme

Approved by

Paul Neeme
Mark S. Sirinides/Ted Neeme

Denver Instrument Company

Certificate of Calibration

Model A-160

Date 11/12/91

Serial Number 6033653

We hereby certify that the referenced instrument was manufactured in the United States and that it has been calibrated to full capacity using NBS Class S-1 weights. This instrument has been fully inspected and has passed all quality tests as specified by Denver Instrument Company quality control guidelines.

To assure proper operation, it may be necessary to recalibrate the instrument periodically using known weights.

Carie Dett

Quality Technician

Diana Dilgoff

Quality Control Manager

Denver Instrument Company

6542 Fyfe Street • Avada, Colorado 80004 • 1-800-821-1185

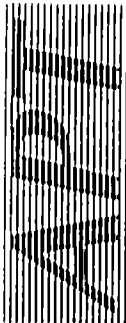
MANUFACTURER'S CALIBRATION CERTIFICATE

The following record shows the accuracy of your digital flowmeter
at tested flow rates compared to NBS (NIST) calibrated standard
TN 242118 TELEDYNE HEM-1A #1337.

CALIBRATION DATE:	07-18-91	PRESSURE (mb):	1004
INTERNAL UNIT #:	10516	SERIAL #:	<u>302143</u>
CALIBRATION FLOW (ml/min)	% ERROR	TEMPERATURE (C):	21
49.28	0.84	REL. HUMIDITY (%):	48
499.12	-0.84		
2982.08	-0.53		

CALIBRATED BY: KTT

SCIENTIFIC INDUSTRIES, INC.
2207 Bluebell Avenue
Boulder, Colorado 80302-8029
Phone 303-443-7087



AIR POLLUTION TESTING, INC.

4535 West 68th Avenue • Westminster, CO 80030 (303) 426-0402 Fax (303) 426-1922

Meter Calibration Data Sheet

Client

Date Pre-Test Cal 7-6-92

Pb (mbar) 839

Date Post-Test Cal 1-17-93

Pb (mbar) 841

Max Vacuum 5 HG

ΔH	V_{meter}	V_{ref}	T_{ref}	T_{inlet}	T_{outlet}	ΔP	Θ	
0.5	30.115	502.765	70	73	72	.12	0	Y_d 1.0447
0.5	40.000	512.743	72	75	74	.12	22	$\Delta H@$ 1.537
0.5	9.885	9.978	71	74	73	.12		
1.0	40.000	512.743	72	75	74	.16		Y_d 1.0434
1.0	52.103	524.915	72	79	77	.16		$\Delta H@$ 1.073
1.0	12.103	12.252	72	77	75.5	.16		
2.5	54.000	526.792	72	79	77	.28		Y_d 1.0786
2.5	68.100	540.955	73	81	79	.28		$\Delta H@$ 1.809
2.5	14.100	14.163	72.5	80	78	.28		$\overline{Y_d} = 1.0389$ $\Delta H@ = 1.683$

ΔH	V_{meter}	V_{ref}	T_{ref}	T_{inlet}	T_{outlet}	ΔP	Θ	
.5	233.185	951.220	68	48	45	.08	0	Y_d 1.065
.5	250.550	969.090	70	68	59	.08	40	$\Delta H@$ 1.62
	16.865	17.87	69	58	52	.08	40	
1.5	250.050	969.090	70	75	64	.16	0	Y_d 1.071
1.5	264.818	984.522	70	81	68	.16	21	$\Delta H@$ 1.78
	14.768	15.422	70	78	66	.16	21	
3.0	264.818	984.522	70	81	68	.29	0	Y_d 1.065
3.0	280.000	1000.422	70	89	74	.29	15	$\Delta H@$ 1.73
	15.242	15.900	70	85	71	.29	15	$\overline{Y_d} = 1.067$ $\Delta H@ = 1.71$