



Ambient Engineering Inc.

1145 Bordentown Avenue
Parlin, New Jersey 08859
(201) 727-8333

ENVIRONMENTAL ENGINEERING/SYSTEMS

AP-42 Section 9.13.2
Reference 8
Report Sect. _____
Reference _____

WA: _____
WASTE _____
NOISE _____
ENERGY _____
O.S.H.A. _____

50003

Note: This is a reference cited in AP 42, *Compilation of Air Pollutant Emission Factors, Volume I Stationary Point and Area Sources*. AP42 is located on the EPA web site at www.epa.gov/ttn/chief/ap42/

The file name refers to the reference number, the AP42 chapter and section. The file name "ref02_c01s02.pdf" would mean the reference is from AP42 chapter 1 section 2. The reference may be from a previous version of the section and no longer cited. The primary source should always be checked.

COMPLIANCE STACK SAMPLING REPORT For

Hills Brothers Coffee, Inc.
535 River Road
Edgewater, NJ 07020

Source Tested:

Afterburner #23 Inlet/Outlet
Hills Brothers Coffee, Inc.
Edgewater, NJ

In Fulfillment of Purchase Order No. 32065

Ambient Engineering Project No. 859

Test Date: August 31, 1988

Report Date: September 23, 1988



Ambient Engineering Inc.

1145 Bordentown Avenue
Parlin, New Jersey 08859
(201) 727-8333

ENVIRONMENTAL ENGINEERING/SYSTEMS

AIR
WATER
WASTE
NOISE
ENERGY
O.S.H.A.

STACK SAMPLING REPORT FOR
Hills Brothers Coffee, Inc.

535 River Road

Edgewater, NJ 07020

On Afterburner #23 Inlet/Outlet

At Hills Brothers Coffee, Inc., Edgewater, NJ

INTRODUCTION

The above referenced stack was sampled for particulates, total hydrocarbons as methane, and carbon monoxide emissions on August 31, 1988. This report contains the following information.

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SUMMARY

The following results were obtained:

Run No.	<u>INLET</u>		
	1	2	3
Date	8/31/88	-----	-----
Time	0834-0938	1644-1747	1900-2005

Emissions DataParticulate Emissions

pounds/hour	2.55	2.61	2.48
grains/dscf	0.101	0.106	0.108
grains/scf	0.082	0.085	0.084

Total Hydrocarbons
(as methane)

pounds/hour	3.83	8.73	5.38
ppmv (wet)	420	975	625
ppmv (dry)	520	1200	800

Carbon Monoxide

pounds/hour	6.0	7.9	7.2
ppmv (wet)	380	510	480
ppmv (dry)	460	630	610

SUMMARY (continued)

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Run No.	OUTLET		
	1	2	3
Date	8/31/88 -----		
Time	0833-0937	1642-1745	1849-2005
<u>Emissions Data</u>			
<u>Particulate Emissions</u>			
pounds/hour	0.26	0.07	0.14
grains/dscf	0.007	0.002	0.004
grains/scf	0.006	0.002	0.003
<u>Total Hydrocarbons*</u>			
<u>(as methane)</u>			
pounds/hour	1.40-1.48	0.99-1.08	0.63-0.72
ppmv (wet)	110-117	74-81	48-54
ppmv (dry)	134-142	90-98	58-66
<u>Carbon Monoxide</u>			
pounds/hour	0.04	0.02	0.02
ppmv (wet)	1.8	1.1	1.1
ppmv (dry)	2.2	1.3	1.3

* By New Jersey Test Method 3. If a range of values is shown, the range was determined by assuming the non-detected hydrocarbons in a portion of the catch was (1) zero or (2) the detection limit of the analytical instrument.

Samples from this project will be retained for sixty days from the date of this report unless otherwise directed.



Ambient Engineering Inc.

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PERSONNEL AND CERTIFICATIONS

Field sampling on this project was performed by:

T.F. Mattei	S.J. Culmo
P.F. Marshall	A.W. McNeel

Laboratory work on this project was performed by:

A.W. McNeel	R.N. Schaffer
-------------	---------------

Calculations and report preparations were by:

P.F. Marshall

The testing was observed by: NJ DEP Representative:

Staffort Stewart	NJ DEP.
Gary Andrew	NJ DEP.

This Report is submitted by:

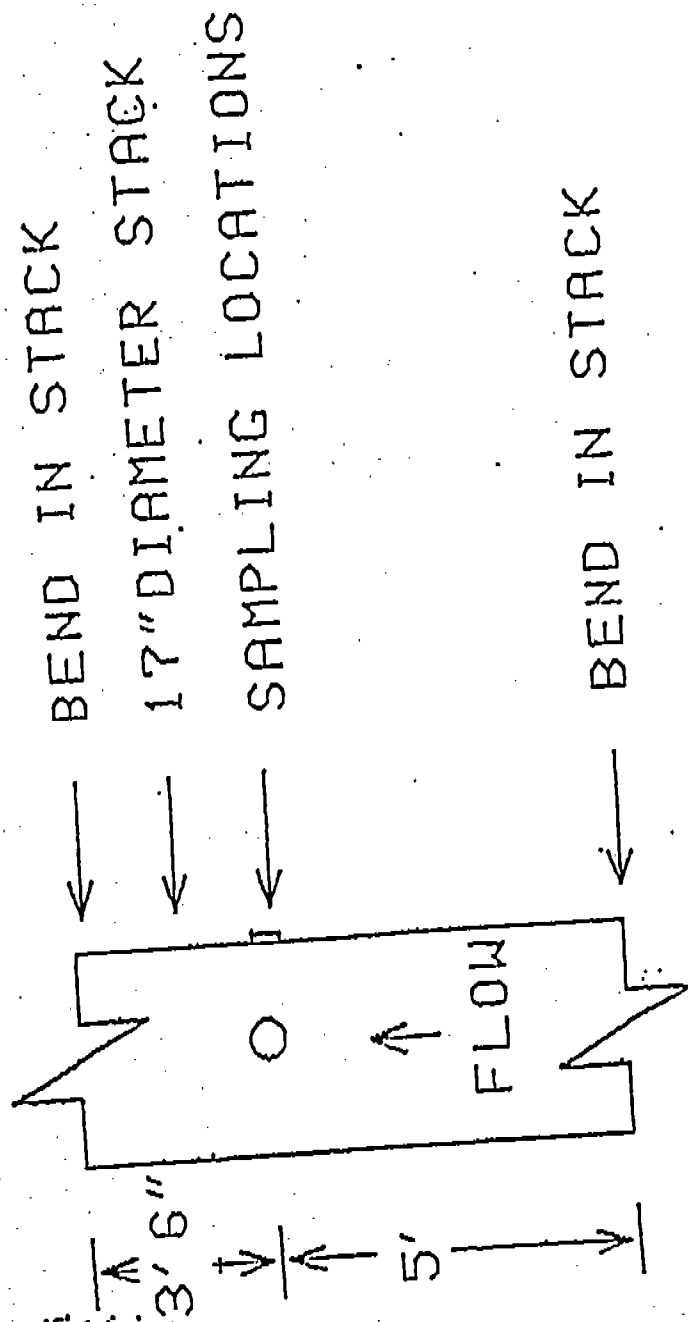
Barry Hull
Project Manager

Professional Engineer Certification

I am in responsible charge of Ambient Engineering's stack test work, and have discussed and reviewed the procedures and results of this set of tests with the relevant field and laboratory personnel.

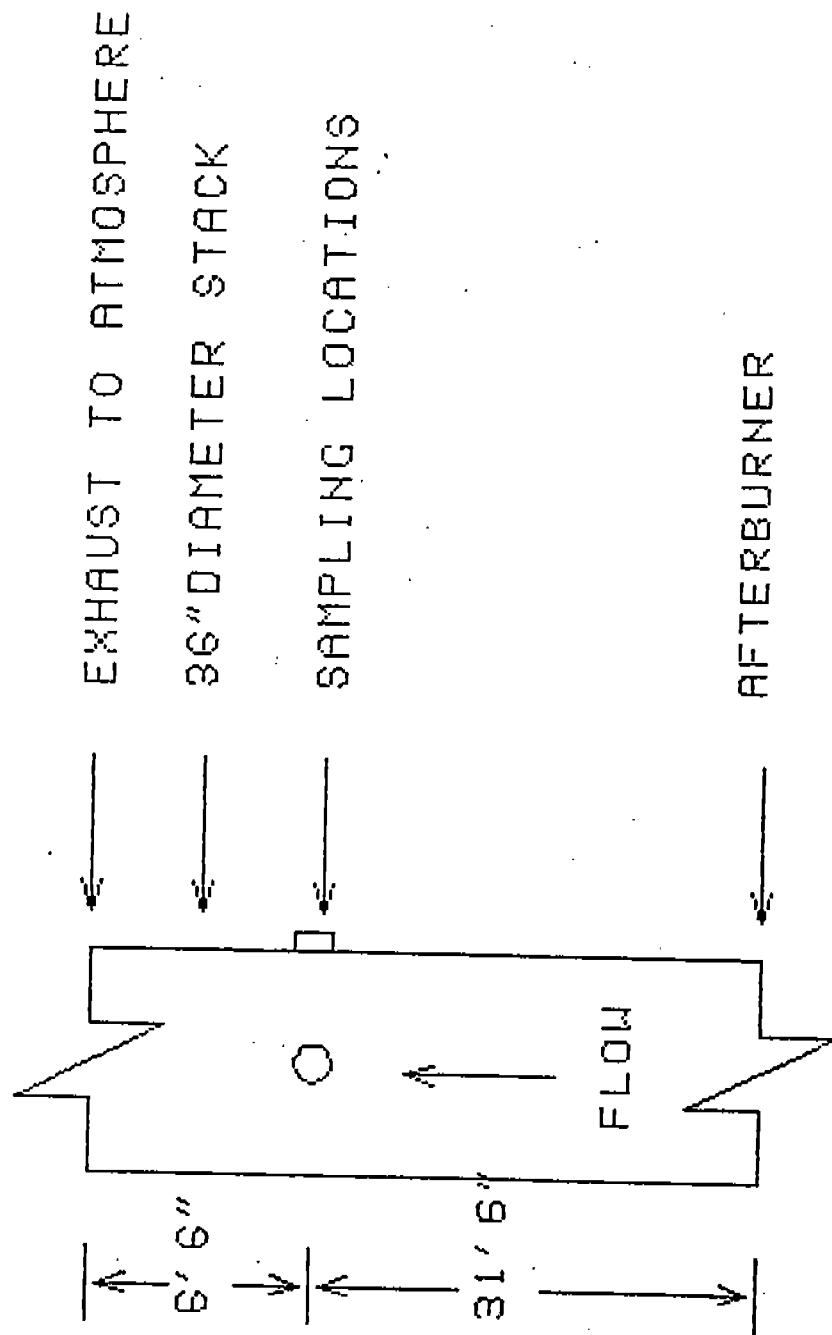
John Yavorsky, Ph.D., PE
NJ License: 28675

HILLS BROS. COFFEE
AFTER BURNER INLET
STACK 23



EPA DISTANCE "A": >2.00
EPA DISTANCE "B": 3.53
TRAVERSE POINTS: 24

HILLS BROS. COFFEE
AFTERBURNER OUTLET
STACK 22 AND 23



EPA DISTANCE "A": 2.17
EPA DISTANCE "B": 10.5
TRAVERSE POINTS: 12

VELOCITY AND FLOW RATE DATA - Inlet

Run No.	1	2	3
Date	8/31/88 -----		
Time	0834-0938	1644-1747	1900-2005
Stack Diameter (in)	17 -----		
Stack Cross Section (sq ft)	1.58 -----		
Barometric Pressure ("Hg)	29.98 -----		
Average Stack Temperature (°F)	525	551	590
Stack Pressure ("H ₂ O-gage)	4.2	4.0	4.1
Moisture (% vol)	18.0	19.2	21.6
Average Velocity (ft/sec)	70.02	71.20	71.06
Actual Flow Rate (acfm)	6,620	6,730	6,720
Standard Flow Rate (scfm)	3,610	3,570	3,430
Dry Standard Flow Rate (dscfm)	2,960	2,880	2,690

Standard Conditions are 70°F, 29.92 "Hg.

VELOCITY AND FLOW RATE DATA - Outlet

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Run No.	1	2	3
Date	8/31/88	-----	-----
Time	0833-0937	1642-1745	1849-2005
Stack Diameter (in)	36	-----	-----
Stack Cross Section (sq ft)	7.07	-----	-----
Barometric Pressure ("Hg)	29.98	-----	-----
Average Stack Temperature (°F)	1205	1210	1210
Stack Pressure ("H ₂ O-gage)	-0.11	-0.14	-0.13
Moisture (% vol)	17.7	17.3	18.0
Average Velocity (ft/sec)	37.45	39.50	39.35
Actual Flow Rate (acfm)	15,900	16,700	16,700
Standard Flow Rate (scfm)	5,060	5,320	5,290
Dry Standard Flow Rate (dscfm)	4,170	4,400	4,340

Standard Conditions are 70°F, 29.92 "Hg.

CYCLONIC FLOW - Inlet

<u>Point</u>	<u>Angle, Degrees</u>	
	<u>Port A</u>	<u>Port B</u>
1	0	2
2	5	3
3	5	5
4	7	9
5	7	9
6	8	4
7	6	7
8	10	7
9	10	8
10	8	4
11	0	4
12	<u>3</u>	<u>3</u>

Avg 5.6

CYCLONIC FLOW - Outlet

<u>Point</u>	<u>Angle, Degrees</u>	
	<u>Port A</u>	<u>Port B</u>
1	3	4
2	4	3
3	4	3
4	2	3
5	2	2
6	<u>2</u>	<u>2</u>

Avg 2.8

STACK GAS COMPOSITION - Inlet

Run No.	1	2	3
Date	8/31/88	-----	-----
Time	0834-0938	1644-1747	1900-2005

% By Volume
(Dry Basis)

ONSITE FYRITE

CO ₂	3.0	3.0	3.0
O ₂	17.0	17.0	17.0
N ₂ (By Difference)	80.0	80.0	80.0

LAB ORSAT

CO ₂	2.7	2.7	2.9
O ₂	17.0	16.8	16.5
N ₂ (By Difference)	80.3	80.5	80.6

STACK GAS COMPOSITION - Outlet

Run No.	1	2	3
Date	8/31/88	-----	-----
Time	0833-0937	1642-1745	1849-2005

% By Volume
(Dry Basis)ONSITE FYRITE

CO ₂	0.0	0.0	0.0
O ₂	21.0	21.0	21.0
N ₂ (By Difference)	79.0	79.0	79.0

LAB ORSAT

CO ₂	0.1	0.1	0.1
O ₂	21.1	21.1	21.1
N ₂ (By Difference)	78.8	78.8	78.8

PARTICULATE AND SULFUR OXIDE EMISSIONS - Inlet

Run No.	1	2	3
Date	8/31/88 -----		
Time	0834-0938	1644-1747	1900-2005

Sampling Data

Nominal Nozzle Size (in)	1/4 -----		
No. of Sampling Points	24 -----		
Sampling Time (min)	60 -----		
Sample Volume (dscf)	39.8	39.3	35.0
% Isokinetic	99	98	94

Emissions DataParticulate Emissions

pounds/hour	2.55	2.61	2.48
grains/dscf	0.101	0.106	0.108
grains/scf	0.082	0.085	0.084

PARTICULATE AND SULFUR OXIDE EMISSIONS - Outlet

Run No.	1	2	3
Date	8/31/88 -----		
Time	0833-0937	1642-1745	1849-2005

Sampling Data

Nominal Nozzle Size (in)	7/16-----		
No. of Sampling Points	12 -----		
Sampling Time (min)	60 -----		
Sample Volume (dscf)	40.1	42.4	41.9
% Isokinetic	103	104	99

Emissions Data
Particulate Emissions

pounds/hour	0.26	0.07	0.14
grains/dscf	0.007	0.002	0.004
grains/scf	0.006	0.0016	0.003

HYDROCARBON EMISSIONS AND CARBON MONOXIDE - Inlet

Run No.	1	2	3
Date	8/31/88 -----		
Time	0834-0938	1644-1747	1900-2005

Sampling Data

No. of Sampling Points	1 -----
Sampling Time (min)	60 -----
Sample Volume (dscf)	2.12 -----

Emissions DataTotal Hydrocarbons(as methane)

pounds/hour	3.83	8.73	5.38
-------------	------	------	------

ppmv (wet)	420	975	625
------------	-----	-----	-----

ppmv (dry)	520	1200	800
------------	-----	------	-----

Carbon Monoxide

pounds/hour	5.97	7.91	7.18
-------------	------	------	------

ppmv (wet)	380	510	480
------------	-----	-----	-----

ppmv (dry)	460	630	610
------------	-----	-----	-----

HYDROCARBON EMISSIONS AND CARBON MONOXIDE - Outlet

Run No.	1	2	3
Date	8/31/88 -----		
Time	0833-0937	1642-1745	1849-2005

Sampling Data

No. of Sampling Points	1 -----
Sampling Time (min)	60 -----
Sample Volume (dscf)	2.12 -----

Emissions DataTotal Hydrocarbons*
(as methane)

pounds/hour	1.40-1.48	0.99-1.08	0.63-0.72
ppmv (wet)	110-117	74.4-81.2	47.6-54.3
ppmv (dry)	134-142	90.0-98.2	58.0-66.2

Carbon Monoxide

pounds/hour	0.04	0.02	0.02
ppmv (wet)	1.81	1.07	1.07
ppmv (dry)	2.20	1.30	1.30

* By New Jersey Test Method 3. If a range of values is shown, the range was determined by assuming the non-detected hydrocarbons in a portion of the catch was (1) zero or (2) the detection limit of the analytical instrument.



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ENVIRONMENTAL ENGINEERING/SYSTEMS

AIR
WATER
WASTE
NOISE
ENERGY
O.S.H.A.

Hills Bros. Coffee, Inc.
535 River Road
Edgewater, NJ 07020

PROCESS DESCRIPTION

Stack #23

Hills Brothers Coffee, Inc. is a world leader in the production of fine coffee for sale in retail and commercial establishments. Coffee beans are purchased world wide and shipped to Hills Brothers, Edgewater, New Jersey plant for processing and packaging.

Stack 23R is the emission to atmosphere point for the coffee Roaster and Stack 23C is the outlet for air used to cool the Roasted Beans.

The process consists of a mixture of green coffee beans being fed on a continuous basis (up to 16 hours per day) into roaster 23. The beans are weighed and fed by gravity on the roaster belts. The feed rate is between 150-170#/minute. Only green coffee beans are roasted in these ovens and the control feed is in the main control room.



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Hills Bros. Coffee, Inc
Process Description
Stack #23/AE859(8)

Roaster Stack outlet flow rates:

	<u>Run 1</u>	<u>Run 2</u>	<u>Run 3</u>
Actual Flow Rate, ACFM	15875.48	16747.00	16682.61
Standard Flow Rate, SCFM	5061.60	5323.35	5291.38
Dry Standard Flow Rate, DSCFM	4167.66	4402.18	4339.71

CONTROL APPARATUS ON SOURCE

The Smoke reduction system consists of a variable speed fan, dampers and ductwork that remove smoke from the roaster to a natural gas fired afterburner. By designing this system to provide a negative pressure inside the roaster, smoke is prevented from leaking into the cooler. A low profile hood over the coffee conveying pan between the roaster and cooler reduces the volume of air over the beans. Combined with negative pressure within the roaster, this creates an air velocity over the roasted beans that will further reduce the smoke introduced into the cooler.



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Hills Bros. Coffee, Inc
Process Description
Stack #23/AE859(8)

Roaster Stack #23 was tested on August 31, 1988. The following process data was recorded during the testing"

Roaster #23 Stack:	<u>Gas Meter</u>		<u>Gas Meter</u>
<u>Afterburner</u>	<u>Run 1</u>	<u>Roaster</u>	<u>Run 1</u>
Finish 0938	74990	Finish 0942	42570
Start 0835	<u>74930</u>	Start 0846	42525
Total 63 min	60	Total 56 min	45
 <u>Afterburner</u>	 <u>Run 2</u>	 <u>Roaster</u>	 <u>Run 2</u>
Finish 1745	75473	Finish 1749	42943
Start 1641	<u>75410</u>	Start 1643	42890
Total 64 min	63	Total 66 min	53
 <u>Afterburner</u>	 <u>Run 3</u>	 <u>Roaster</u>	 <u>Run 3</u>
Finish 2005	75605	Finish 2005	43045
Start 1845	<u>75532</u>	Start 1848	42989
Total 80 min	73	Total 77 min	56

*Natural gas meter readings in nearest 100 cu ft.

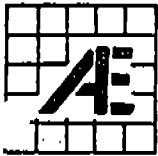
Production of 165#/min was constant during the testing.

Note: The roaster #23R was in continuous operation during the stack testing. The production rate remained at 165 #/min and was monitored by the Dep. representative Mr. M. Klein, of the Metropolitan Regional Office.

ALLOWABLE EMISSIONS

The following allowable emissions are based on our understanding of the applicable regulatory rules and regulations. Since we are not always privy to the situation, these should not be accepted without confirmation from relevant sources.

<u>Particulate</u>	<u>Reference</u>	<u>Allowable</u>
Federal Regulations		
State Regulations	<u>7:27-6.2</u>	<u>0.02 grains/SCF</u>
State Permit		
<u>Sulfur Dioxide</u>		
Federal Regulations		
State Regulations		
State Permit		
<u>Sulfur Trioxide and Sulfuric Acid</u>		
Federal Regulations		
State Regulations		
State Permit		
<u>Nitrogen Oxides</u>		
Federal Regulations		
State Regulations		
State Permit		
<u>Hydrocarbon (VOS, VOC)</u>		
Federal Regulations		
State Regulations		
State Permit		
<u>Other: Opacity</u>		
Federal Regulations		
State Regulations	<u>7:27-6.2</u>	<u>20%</u>
State Permit		



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STACK TEST PROTOCOL SUBMITTAL

NEW JERSEY DEPARTMENT OF
ENVIRONMENTAL PROTECTION
Technical Services Section
380 Scotch Road
W. Trenton, NJ 08628

RE: HILLS BROTHERS COFFEE, INC.
535 River Road
Edgewater, NJ 07020

Contact: Barry Hull
Phone No: 201-727-8333

ATTN: Edward Choromanski

AE Project No. 859

This protocol is submitted for stack testing planned by Ambient Engineering, Inc. for the above referenced client.

Source to be tested: Afterburner Inlet and Outlet
ID No.: #22 Stack

Approximate Date of Testing: August 10 and 11, 1988

INLET

Isokinetic Testing

Stack diameter	17"
Nearest upstream disturbances	3'
Nearest downstream disturbances	6'
EPA Distance "A" >2.00 EPA Distance "B"	4.23
Proposed number of sampling points	24
Proposed time per sampling point	3 minutes
Proposed total stack gas sample size	35.00 dry standard ft ³

Hydrocarbon Testing

Proposed number of sampling points	1
Proposed time per sampling point	60 minutes
Proposed total stack gas sample size	2.12 dry standard ft ³

Outlet

Isokinetic Testing

Stack diameter	36"
Nearest upstream disturbances	6'6"
Nearest downstream disturbances	31'6"
EPA Distance "A" 2.17 EPA Distance "B"	10.5
Proposed number of sampling points	12
Proposed time per sampling point	5 minutes
Proposed total stack gas sample size	35.00 dry standard ft ³

Hydrocarbon Testing

Proposed number of sampling points 1
Proposed time per sampling point 60 minutes
Proposed total stack gas sample size 2.12 dry standard ft³

Source Operation Record Keeping

Responsibility of A Owner B RECON

 A Production rate
 Fuel usage
 Incineration feed rate
 Steam production
 A Operating parameters (temperatures, pressures, flows, etc.)
 Other

ANALYTICAL PROGRAMHydrocarbon and Carbon Monoxide

Sample stack gas will be pulled through hydrocarbon-free water to remove condensibles, and pumped into an 80 liter Tedlar gas bag. The entire sampling train shall consist of teflon, glass, stainless steel and Tedlar (diagram of sampling train follows). Sampling rates will be determined by use of an in-line rotameter which will be calibrated onsite using a dry gas meter. The sampling train will be run during the particulate testing.

LABORATORY PROCEDURES

Samples will be analyzed as follows:

1. Condensible material recovered in the impinger catches will be determined by a gas chromatograph equipped with a flame ionization detector for determination of total hydrocarbons as methane with known standards.
2. Gas bag samples will be directly injected into the GIC/FID via a calibrated sample loop. Concentrations will be determined as above. Concentrations of both phases will be totaled and used to calculate emissions. The gas bags will then be analyzed for carbon monoxide using a Thermo Electron Model 48 Non-Dispersive Infrared (NDIR) analyzer using specific standards. Copies of chromatograms will be included in our final report showing identified responses plus any other unidentified peaks.

Particulate

Three (3) one-hour compliance tests will be conducted for particulates using New Jersey Air Test Method 1. Temperatures of the stack, probe, filter inlet, filter box and filter outlet will be recorded. Flow rates, O₂, CO₂, N₂ (by difference) will also be recorded. Impinger Numbers 1 and 2 will have 100 mls. each H₂O. Impinger Number 3 empty. Impinger Number 4 200 gms. silica gel. Non-cyclonic flow will be field verified. Calibration data will be made available to the onsite observer.

Total Hydrocarbons

New Jersey Air Test Method 3 will be utilized to determine total hydrocarbon emissions. Concentrations will be expressed as equivalent methane.

Opacity

US EPA Method 9 will be utilized to determine outlet opacity.

Meter Box No. 4 Barometric Pressure (Pb) 29.96 "Hg Calibrated by: SJC

Dry Gas Meter No. 578753

Ambient Temperature (Tamb) 82.2°F Date: 6-17-88

ΔH	Meter Temperature (T _m)				METER READING (V _m)		Time @ seconds	ΔH @	Difference From ΔH @
	Inlet (°F)	Outlet (°F)	Avg (°F)	T _m +460 (°F)	Final	Initial			
Orifice Setting									
0.25						5			
0.50	84	82	83	543	531.960	531.205	755	2.02	
0.75	87	82	84.5	544.5	523.187	524.259	928	2.01	.01
1.00	87	82	84.5	544.5	524.618	523.550	1.068	2.02	.02
1.50	89	83	86	546	526.045	524.760	1.285	2.11	.11
2.00	90	84	87	547	527.762	526.254	1.508	2.05	.05
2.50	90	83	86.5	546.5	529.187	528.011	1.678	2.03	.07
3.00									

$$\Delta H @ = \frac{0.0317 (\Delta H)}{P_b (T_{amb} + 460)} \times \left[\frac{(T_m + 460) (C \oplus)}{(V_m) (Y\text{-factor}) (60)} \right]^2$$

Y Factor - Dry Gas Meter Correction Factor 30

Note: Difference From ΔH @ not to exceed ± 0.15

PROOF AND DIFFERENTIAL TEST RECORD

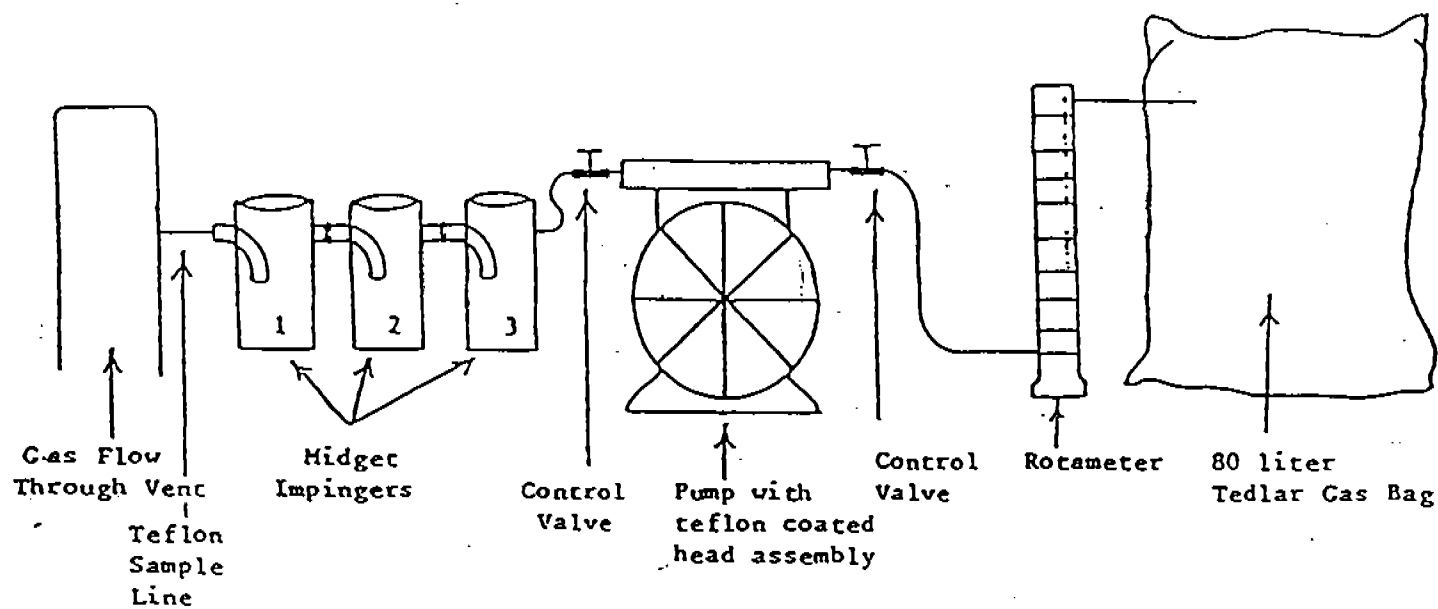
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Meter Size S-130 S-A90 Date Received 8-27-87 Inspector J. Soprano
 Date Tested 9-2-87 New Repaired ✓ Manufacturer Rockwell + A
 Prover No. 1264 Temperatures: Room Air 79 F.
 Total Meters this Page 3 Oil 79 F.
 Prover Air 79 F.

Temp. Comp. Meters: $\frac{\text{Abs. Base Temp.}}{\text{Abs. Prover Temp.}} \times \text{Uncorr. \% Proof} = \text{Corr. \% Proof}$

Meter No.	Repair Class	Percent Proof		Differential Maximum	Remarks
		Check	Open		
716691	INTEST	99.8	100.7	20	Uncorr. $\frac{AS}{\%}$ Proof AS FOUND
					Corr. $\frac{AS}{\%}$ Proof
38949	INTEST	106.2	103.8	36	Uncorr. $\frac{AS}{\%}$ Proof AS FOUND
					Corr. $\frac{AS}{\%}$ Proof
175176	INTEST	98.8	98.8	28	Uncorr. $\frac{AS}{\%}$ Proof AS FOUND
					Corr. $\frac{AS}{\%}$ Proof
					Uncorr. $\frac{AS}{\%}$ Proof
					Corr. $\frac{AS}{\%}$ Proof
716691	ADJUST	100.0	100.2	20	Uncorr. $\frac{AS}{\%}$ Proof CALIBRATED
					Corr. $\frac{AS}{\%}$ Proof
38949	VALUE	100.0	100.1	36	Uncorr. $\frac{AS}{\%}$ Proof CALIBRATED
					Corr. $\frac{AS}{\%}$ Proof
175176	ADJUST	100.2	100.2	28	Uncorr. $\frac{AS}{\%}$ Proof CALIBRATED
					Corr. $\frac{AS}{\%}$ Proof

DIAGRAM OF SAMPLING TRAIN



- Midget impingers - 1 and 2 with distilled water, and 3 empty.
- Condenser section in ice bath.
- Complete sample train to be leak checked using a soap film bubble meter or a dry gas meter prior to and after testing.
- Rotameter settings (sampling rate of assembled train) to be carefully calibrated with a soap film meter.

STACK TESTING PROCEDURES CHECKLIST

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Particulate

Emissions: ☐ US EPA 5
☐ US EPA 17
☒ N.J. Method 1
☐ N.J. Method 5 (draft)
☐ Plus impinger catch
☐ Plus aqueous and organic impinger catch
☐ Other Pyrex glass
 Probe Material

Velocity: ☐ Standard pitot tube and manometer
☒ "S" pitot tube and manometer
☐ Other:
☒ Cyclonic Flow Check ☒ Yes ☐ No

Temperature: ☒ Thermocouple
☐ Temperature gage
☐ Process indicator

Gas

Composition: ☒ Onsite fyrite
☐ Grab sample and lab orsat
☐ Integrated sample and lab orsat
☒ Integrated and traversed sample and lab orsat
☐ Oxygen by Infrared Industries 2200 Electrochemical Analyzer

Particle

Sizing: ☐ Instack cascade impactor
☐ Heated out of stack cascade impactor
☐ Plus impinger catch
☐ Plus aqueous and organic impinger catch

Sulfur Oxide

Emissions: ☐ US EPA 6
☐ US EPA 8
☐ Sulfite Corrections Made
☐ Controlled condensation for SO₃

Nitrogen Oxide

Emissions: ☒ US EPA 7 ☐ A, ☐ B, ☐ C, ☒ D, ☐ E
☐ Chemiluminescent monitor
☐ US EPA 20 (Chemiluminescent Monitor)

Hydrogen Chloride (HCl)

Emissions: ☐ API 767-54
☐ CL⁻ analysis of particulate test wet catch
☐ Other

Hydrocarbon

Emissions: ☒ N.J. Method 3
☐ RECON Method 2
☐ Integrated gas bag direct and lab GC
☐ Grab sample gas bag direct and lab GC
☐ Onsite GC direct ☐ detector
☐ Onsite Continuous Monitor (FID)

Metal Emissions ☐ AA determination on filter and probe wash
☐ AA determination on impinger catch

Carbon Monoxide

Emissions: ☒ Thermal Conductivity analysis of "Gas Composition" sample(s)
☐ Onsite Continuous Monitor

Opacity:

☐ N.J. Method 2
☒ U.S. EPA Method 9

Calibrations: Dry gas meters and orifice, pitot tubes, thermocouples and nozzle calibrations will be supplied with the test report unless test is unofficial.

Comments:

SELECTED NOMENCLATURE

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time	= military time
min	= minutes
°F	= degrees Fahrenheit
°C	= degrees Centigrade
in. ₂ O	= inches water (pressure or vacuum)
in. Hg	= inches mercury (pressure or vacuum)
mm Hg	= millimeters of mercury (pressure or vacuum)
psig	= pounds of pressure per square inch-gage
sq ft	= square feet
in	= inches
micron	= 10 ⁻⁶ meters
ft/sec	= feet per second
ft/min	= feet per minute
acfm	= cubic feet per minute of total gas flow at flowing conditions
scfm	= cubic feet per minute of total gas flow at 70°F, 29.92"Hg
dscfm	= dry cubic feet per minute of dry gas flow at 70°F, 29.92"Hg
pounds/hour	= pounds per hour
pounds/hour	= pounds per hour
BTU/hr	= British thermal units per hour
%	= volume per cent when referred to gases and water vapor
	= weight percent for solids, liquids
% vol	= volume per cent
% wgt	= weight percent
ppmv	= volumes of gaseous contaminants per million volumes of total gas
grains	= grams x 15.4
ug	= micrograms = 10 ⁻⁶ grams
mg	= milligrams = 10 ⁻³ grams
grains/dscf	= grains of pollutants per cubic foot of dry stack gas at 70°F, 29.92 "Hg
gr/dscf	= grains/dscf
ug/m ³	= micrograms of pollutants per cubic meter of total stack gas at 25°C, 760 mm Hg
mg/l	= milligrams/liter of liquid = ppm by weight if specific gravity of liquid = 1.0
C	= elemental carbon
CO ₂	= carbon dioxide
	= elemental hydrogen
	= molecular hydrogen
H ₂ O	= water
N	= elemental nitrogen
N ₂	= molecular nitrogen
NO _x = NO + NO ₂	= nitrogen oxides = nitric oxide plus nitrogen dioxide reported as equivalent nitrogen dioxide
S	= elemental sulfur
SO ₂	= sulfur dioxide
SO ₃	= sulfur trioxide
SO ₄	= sulfate
H ₂ SO ₄	= sulfuric acid
H ₂ S	= hydrogen sulfide
Cl	= elemental chlorine or chloride
Cl ₂	= molecular chlorine
HCl	= hydrogen chloride
F	= elemental fluorine or fluoride
CH ₄	= methane
O	= elemental oxygen
O ₂	= molecular oxygen
A	= argon
<	= less than; represents the minimum detectability limits
≤	= equal to or less than
ND	= none detected

Front half (dry catch particulate) = particulate matter collected in/on nozzle, probe, cyclone, flask heated hose, and filter of EPA sampling train

Back Half (wet catch particulate) = material collected in impingers after filter of EPA sampling train

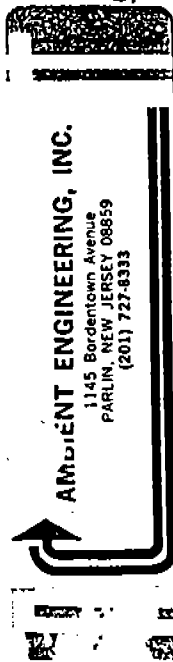
Organic wet catch = residue after low temperature (70°F) evaporation of ether/chloroform used to extract soluble materials from the wet catch

Aqueous wet catch = residue after high temperature (220°F) evaporation of water left after ether/chloroform extraction

Combustibles = volatiles = loss on heating @ 550°C after drying @ 100°C

Ash = residue after heating @550°C

CALIBRATION DATATest Equipment CalibrationData Sheets Follow



AMBIENT ENGINEERING, INC.
1145 Bordentown Avenue
PARLIN, NEW JERSEY 08859
(201) 727-8333

Meter Orifice Calibration Form (L-32)

Meter Box No. 2

Barometric Pressure (Pb) 29.95 Hg

Calibrated by: SJC

Dry Gas Meter No. 41740

Ambient Temperature (Tamb) 70 °F

Date: 6-28-88

ΔH	Meter Temperature (Tm)		METER READING (Vm)		Time @ seconds	ΔH @	Difference From ΔH @
	Inlet (°F)	Outlet (°F)	Avg (°F)	Final Initial Difference (ft³)			
Orifice Setting							
0.25							
0.50	84	72	78	538	162.846	162.106	.74
0.75	81	72	78	538	163.961	163.031	.930
1.00	84	73	78.5	538.5	165.368	164.294	1.074
1.50	85	74	79.5	539.5	166.819	165.536	1.283
2.00	88	74	81	541	168.992	167.512	1.48
2.50	88	74	81	541	170.813	169.163	1.65
3.00							

Calculation

$$\Delta H @ = \frac{0.0317 (\Delta H)}{P_b (T_{amb} + 460)} \times \left[\frac{(T_m + 460) (C \cdot \text{cor})}{(V_m) (Y\text{-factor}) (60)} \right]^2$$

Avg.

2.05

28

Y Factor - Dry Gas Meter
Correction Factor

PROOF AND DIFFERENTIAL TEST RECORD

29

Meter Size S-190 T.C Date Received 8-27-87 Inspector J. S. PRA:15

Date Tested 9-1-87 New Repaired Manufacturer Bo Kwell

Prover No. 1264 Temperatures: Room Air 77 F.

Total Meters this Page Oil 77 F.

Prover Air 77 F.

Temp. Comp. Meters: Abs. Base Temp.
Abs. Prover Temp. x Uncorr. % Proof = Corr. % Proof

Meter No.	Repair Class	Percent Proof		Differential Maximum	Remarks
		Check	Open		
59319	TEST	101.8	101.0	26	Uncorr. AS FOUND % Proof
					Corr. % Proof
21740	TEST	101.6	101.3	40	Uncorr. AS FOUND % Proof
					Corr. % Proof
					Uncorr. % Proof
					Corr. % Proof
					Uncorr. % Proof
					Corr. % Proof
					Uncorr. % Proof
					Corr. % Proof
59219	ADJUST	99.8	99.9	26	Uncorr. AS % Proof CALIBRATED
					Corr. % Proof
21741	ADJUST	100.6	100.3	40	Uncorr. AS % Proof CALIBRATED
					Corr. % Proof

Date 12/24/87 Thermocouple number 45
Ambient temperature 21 °C Barometric pressure 30.46 in. Hg
Calibrator TPIB Reference: mercury-in-glass ASTM
other _____

Reference point number	Source ^a (specify)	Reference thermometer temperature, °C	Thermocouple potentiometer temperature, °C	Temperature difference, % ^b
0°	ICE WATER	0.0	0.2	0.1
100°	boiling WATER	100.5	101.3	0.2
—	boiling cooking oil			

^aType of calibration system used.

^b
$$\left[\frac{(\text{ref temp, } ^\circ\text{C} + 273) - (\text{test thermom temp, } ^\circ\text{C} + 273)}{\text{ref temp, } ^\circ\text{C} + 273} \right] 100 \leq 1.5\%$$

Figure 2.5 Stack temperature sensor calibration data form.

CLIENT: HILLS BROS.

Date: 09/19/88

Time: 10:21 AM

Delta H (IN H2O)	Meter Temp (F)		Stack Temp (F)
	IN	OUT	
1.70	87.00	86.00	1194.00
1.80	100.00	88.00	1212.00
1.90	102.00	89.00	1225.00
1.70	103.00	91.00	1214.00
1.60	103.00	92.00	1189.00
1.10	105.00	93.00	1185.00
1.55	105.00	96.00	1206.00
1.90	107.00	96.00	1224.00
1.90	107.00	97.00	1234.00
1.70	107.00	98.00	1218.00
1.30	109.00	99.00	1177.00
0.98	109.00	100.00	1175.00

AVERAGES

DELTA H = 1.594167 IN H2O

METER TEMP. = 98.70834 F

STACK TEMP. = 1204.417 F

CLIENT: HILLS BROS.

Date: 09/19/88

Time: 10:21 AM

AVERAGE VELOCITY PRESSURE

<u>Delta P</u> <u>(IN H2O)</u>	<u>Delta P</u> <u>Square Root</u>
0.14	0.37
0.15	0.39
0.16	0.40
0.14	0.37
0.13	0.36
0.10	0.32
0.13	0.36
0.16	0.40
0.16	0.40
0.14	0.37
0.11	0.33
0.08	0.28

THE AVERAGE SQUARE ROOT OF DELTA P = .3634699

SAMPLE LOCATION Outlet
HYDROCARBON PUMP NO. 2

HYDROCARBON SAMPLING DATA

RUN NO. 1

DATE 8/31/88

74

TIME	ROTOMETER SETTING	GAS METER TEMP.	VACUUM "HG	SAMPLE RATE L/M
0833	60	79	1	.933
38	60	79	1	.933
43	60	80	1	.933
48	60	80	1	.933
053	60	80	1	.933
58	60	80	1	.933
0903	Stop for port change at NTH Train			
0907	60	81	1	.933
12	60	81	1	.933
17	60	81	1	.933
22	60	81	1	.933
27	60	81	1	.933
32	60	81	1	.933
0937	end			

PRE-LEAK CHECK end

POST-LEAK CHECK ✓

PUMP CALIBRATION FLOW RATE		CALIBRATION INSTRUMENT	FYRITE
FLOW RATE LITERS/MIN	ROTAMETER SETTING	SOAP FILM BURET DRY GAS METER OTHER	% OXYGEN % CARBON DIOXIDE
.933	60		

CORRECTING ROTOMETER VOLUME TO DRY STANDARD CONDITIONS

$$EQUATION: V_{STD} = V_m \times \frac{P_m}{T_m} \times \frac{T_{STD}}{P_{STD}}$$

WHERE:

- V_m = SAMPLE RATE OF ROTOMETER (L/M)
- T_{STD} = $70^{\circ}F + 460^{\circ}F = 530^{\circ}F$
- P_{STD} = 29.92"HG
- P_m = BAROMETRIC PRESSURE DURING SAMPLING ("HG)
- T_m = TEMPERATURE OF GAS STREAM (+460°F)

$$V_{STD} = \quad \times \left(\frac{\quad}{\quad} \right) \times \frac{(530)}{(29.92)} = \quad$$

$$CF = (V_{STD} \text{ L/MIN}) (3.53 \times 10^{-2} \text{ CF/L}) (60 \text{ MIN/1 HR}) = (\quad) (3.53 \times 10^{-2}) (60)$$

$$= \quad \text{CFH}$$

MOISTURE DETERMINATION

SAMPLE LOCATION OutletRUN NO. 1DATE 8/31/88

CHAIN-OF-CUSTODY SAMPLE NO. _____

	GRAMS	GRAMS
IMPINGER 1	FINAL WEIGHT <u>686.1</u> INITIAL WEIGHT <u>571.5</u> INCREASE	IMPINGER 1 <u>114.6</u>
IMPINGER 2	FINAL WEIGHT <u>739.5</u> INITIAL WEIGHT <u>708.0</u> INCREASE	IMPINGER 2 <u>31.5</u>
IMPINGER 3	FINAL WEIGHT <u>457.3</u> INITIAL WEIGHT <u>480.7</u> INCREASE	IMPINGER 3 <u>7.2</u>
SILICA GEL	FINAL WEIGHT <u>808.2</u> INITIAL WEIGHT <u>788.8</u> INCREASE	SILICA GEL <u>19.4</u>
TOTAL MASS OF WATER CAUGHT		<u>172.7</u> GRAMS

CHAIN-OF-CUSTODY SAMPLE NO. _____

FILTER DIAMETER 4 INCHESFILTER TYPE GFC
 FILTER: FINAL WEIGHT 6230 GMS
 INITIAL WEIGHT 6215 GMS
 INCREASE

0.0015 GRAMS

TOTAL MASS OF PARTICULATE CAUGHT THIS FILTER

IS ICE PRESENT IN THE IMPINGER BATH AT THE END OF THIS SAMPLE? YES _____ NO _____

CALCULATIONS

$$V_{m-std} = 17.65 (V_m) \left(\frac{P_{bar} + \Delta H / 13.6}{T_m + 460} \right) = 17.65 () \left(\frac{+ 13.6}{+ 13.6} \right)$$

$$= 17.65 () () = \text{_____} \text{ FT}^3$$

$$V_{w-std} (H_2O) = \frac{\text{GRAMS COLLECTED}}{21.2 \text{ GRAMS/FT}^3} = \frac{()}{(21.2)} = \text{_____} \text{ FT}^3$$

$$\% H_2O = \frac{(V_{w-std}) 100}{((V_{w-std}) + (V_{m-std}))} = \frac{100 ()}{() ()} = \frac{()}{()} = \text{_____} \%$$

$$\text{MOLECULAR WEIGHT (MW)} = \frac{18 (\% H_2O)}{100} + \frac{\text{DRY MW} (100 - \% H_2O)}{100} = 0.18 () + \frac{() ()}{100}$$

$$\text{VELOCITY (ACTUAL) IN STACK} = 85.48 (C_p) \sqrt{\frac{T_s + 460}{P_s (MW)}} \sqrt{\Delta P} = 85.48 (1.48) \sqrt{\frac{1660}{(163)(28)}} \sqrt{\Delta P}$$

$$V_s = (71.8) \sqrt{1.98 \Delta P} = (71.8)(1.40) \sqrt{\Delta P}$$

$$V_s = () \Delta P = () () = 32.61 \text{ FT/SEC}$$

$$ACFM = (V_s)(60)(CSA) = () (60)() = \text{_____}$$

$$\text{VELOCITY @ Stp } V_{s-std} = V_s (17.65) \left(\frac{P_s}{T_s + 460} \right) = \frac{(376)(17.65)(230)}{1660} = 11.997 \text{ FT/SEC}$$

$$SCFM = (V_{s-std})(CSA)(60) = () () (60) = \text{_____}$$

$$DSCFM = \left(\frac{100 - \% H_2O}{100} \right) (SCFM) = () () = \text{_____}$$

$$\text{NOZZLE VELOCITY @ STD } V_n = \frac{(V_{m-std} + V_{w-std})}{60 (8) A_n} = \frac{(473)}{60 () () (10^{-4})} = \text{_____} \text{ FT/SEC}$$

$$I = \frac{100 V_{n-std}}{V_{s-std}} = \frac{100 ()}{()} = \text{_____} \% \text{ Isokinetic}$$

LAB DATA - EVAPORATIONS

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PLANT Hills Bros.SAMPLE LOCATION #23 OutletRUN NO. 1 FORSAMPLING DATE 8/31/88

OPERATING CONDITION

CHAIN-OF-CUSTODY SAMPLE NO.

ACETONE WASHINGS

GROSS 581.8 GMS
 TOTAL TARE - 409.5 GMS
 SAMPLE (A) NET 172.3 GMS
 AMOUNT EVAPORATED (B) 172.3 GMS
 EVAP. BEAKER NO. _____
 GROSS 97.1463 GMS
 TARE - 97.1301 GMS
 (C) NET 0.0162 GMS

ACETONE BLANK

EVAP. BEAKER NO. _____
 GROSS 97.6580 GMS
 TARE - 97.6583 GMS
 NET 0 GMS
 ACETONE BLANK = NET 0 GMS (D)
 TOTAL AMOUNT EVAPORATED 200 GMS (F)

$$\text{CORRECTED NET (E)} = (C) \cdot (B) \left[\frac{(D)}{(F)} \right]$$

$$= (0.0162) \cdot (172.3) \left[\frac{(0)}{(200)} \right]$$

$$= 0.0162 \text{ GMS (E)} = (C) \cdot B \left[\frac{(D)}{(F)} \right]$$

$$\text{SCALED UP NET} = (E) \left(\frac{A}{B} \right)$$

$$= 0.0162 \left(\frac{172.3}{172.3} \right)$$

$$= 0.0162 \text{ GMS}$$

~~WET CATCH~~

~~GROSS _____ GMS
 TOTAL TARE - _____ GMS
 SAMPLE (A) NET _____ GMS
 AMOUNT EXTRACTED (G) _____ GMS (HLS)
 AMOUNT OF E/C _____ GMS (H)~~

~~WATER PHASE
 EVAP. BEAKER NO. _____
 GROSS _____ GMS
 TARE - _____ GMS
 (J) NET _____ GMS
 WATER BLANK
 (L) = _____ GMS
 100 GMS~~

~~CORRECTED NET
 (N) = J - (G)(L)~~

$$= \text{_____} \left(\frac{\text{_____}}{100} \right)$$

$$= \text{_____} \text{ GMS}$$

$$\text{SCALED UP NET} = (N) \left(\frac{F}{G} \right)$$

$$= \text{_____} \left(\frac{\text{_____}}{\text{_____}} \right)$$

$$= \text{_____} \text{ GMS}$$

~~EC PHASE
 EVAP. BEAKER NO. _____~~

~~GROSS _____ GMS
 TARE - _____ GMS
 (K) NET _____ GMS
 E/C BLANK
 (M) = _____ GMS
 100 MLS~~

~~CORRECTED NET
 (M) = K - (H)(M)~~

$$= \text{_____} \left(\frac{\text{_____}}{100} \right)$$

$$= \text{_____} \text{ GMS}$$

$$\text{SCALED UP NET} = (P) \left(\frac{F}{G} \right)$$

$$= \text{_____} \left(\frac{\text{_____}}{\text{_____}} \right)$$

$$= \text{_____} \text{ GMS}$$

Particulates

Nozzle, Probe, and Acetone Washing .0162 grms

Filter .0015 grms

Enter "0" if no Organic or Aqueous Phase

Aqueous Phase 0 grms

Organic Phase 0 grms

Totals

GRAINS/DSCF = 7.167679E-03

POUNDS/HOUR = .2560486

HIT RETURN TO CONTINUE

78

[illegible]

AirRecon
THREE BRIDGES, NJ

CLIENT: HILLS BROS.

Date: 09/19/88

Time: 10:21 AM

Delta H (IN H2O)	Meter Temp (F)		Stack Temp (F)
	IN	OUT	
1.70	100.00	99.00	1195.00
2.20	100.00	97.00	1217.00
1.90	100.00	96.00	1234.00
1.90	100.00	95.00	1227.00
1.60	100.00	94.00	1197.00
1.20	102.00	94.00	1193.00
1.90	100.00	94.00	1194.00
2.15	103.00	94.00	1227.00
2.15	103.00	93.00	1239.00
1.80	102.00	93.00	1205.00
1.55	101.00	93.00	1194.00
1.10	101.00	92.00	1190.00

AVERAGES

DELTA H = 1.7625 IN H2O

METER TEMP. = 97.75 F

STACK TEMP. = 1209.333 F

CLIENT: HILLS BROS.

Date: 09/19/88

Time: 10:21 AM

AVERAGE VELOCITY PRESSURE

<u>Delta P</u> <u>(IN H2O)</u>	<u>Delta P</u> <u>Square Root</u>
0.16	0.40
0.18	0.42
0.16	0.40
0.16	0.40
0.13	0.36
0.10	0.32
0.16	0.40
0.18	0.42
0.18	0.42
0.15	0.39
0.13	0.36
0.00	0.00

THE AVERAGE SQUARE ROOT OF DELTA P = .383119

HYDROCARBON SAMPLING DATA
 SAMPLE LOCATION OUTLET RUN NO. 2
 HYDROCARBON PUMP NO. 2

DATE 4/31/85

81

TIME	ROTOMETER SETTING	GAS METER TEMP.	VACUUM "HG	SAMPLE RATE L/H
1642	60	78	1	.933
1647	60	79	1	.933
1652	60	79	1	.933
17	60	79	1	.933
1702	60	80	1	.933
1707	60	80	1	.933
1712	60 stop	80	1	
1715	Restart 60	80	1	.933
1720	60	80	1	.933
25	60	80	1	.933
30	60	81	1	.933
35	60	81	1	.933
40	60	81	1	.933

PRE-LEAK CHECK 45

POST-LEAK CHECK ✓

PUMP CALIBRATION FLOW RATE		CALIBRATION INSTRUMENT	FYRITE
FLOW RATE LITERS/MIN	ROTAMETER SETTING	SOAP FILM BURET DRY GAS METER OTHER	% OXYGEN % CARBON DIOXIDE
.933	60		

CORRECTING ROTOMETER VOLUME TO DRY STANDARD CONDITIONS

$$\text{EQUATION: } V_{\text{STD}} = V_m \times \frac{P_m}{T_m} \times \frac{T_{\text{STD}}}{P_{\text{STD}}}$$

WHERE:

V_m = SAMPLE RATE OF ROTOMETER (L/H)
 T_{STD} = $70^{\circ}\text{F} + 460^{\circ}\text{F} = 530^{\circ}\text{F}$
 P_{STD} = 29.92"HG
 P_m = BAROMETRIC PRESSURE DURING SAMPLING ("HG)
 T_m = TEMPERATURE OF GAS STREAM (+460°F)

$$V_{\text{STD}} = \quad \times \left(\frac{\quad}{\quad} \right) \times \frac{(530)}{(29.92)} = \quad$$

$$\text{CF} = (V_{\text{STD}} \text{ L/MIN}) (3.53 \times 10^{-2} \text{ CF/L}) (60 \text{ MIN/1 HR}) = (\quad) (3.53 \times 10^{-2}) (60)$$

= CFH

SAMPLE LOCATION outlet MOISTURE DETERMINATION
 RUN NO. 2
 CHAIN-OF-CUSTODY SAMPLE NO. _____

DATE 8/30/88 82

	GRAMS	GRAMS
IMPINGER 1	FINAL WEIGHT <u>723.3</u> INITIAL WEIGHT <u>686.1</u> INCREASE _____	IMPINGER 1 <u>137.2</u>
IMPINGER 2	FINAL WEIGHT <u>765.9</u> INITIAL WEIGHT <u>739.5</u> INCREASE _____	IMPINGER 2 <u>26.4</u>
IMPINGER 3	FINAL WEIGHT <u>490.2</u> INITIAL WEIGHT <u>482.3</u> INCREASE _____	IMPINGER 3 <u>2.9</u>
SILICA GEL	FINAL WEIGHT <u>829.8</u> INITIAL WEIGHT <u>812.6</u> INCREASE _____	SILICA GEL <u>17.2</u>
TOTAL MASS OF WATER CAUGHT		<u>178.7</u> GRAMS

CHAIN-OF-CUSTODY SAMPLE NO. _____

FILTER DIAMETER 4 INCHES

FILTER TYPE Glass Fiber

FILTER: FINAL WEIGHT 6264 GMS
 INITIAL WEIGHT 6235 GMS
 INCREASE _____

0.0029 GRAMS

TOTAL MASS OF PARTICULATE CAUGHT THIS FILTER

IS ICE PRESENT IN THE IMPINGER BATH AT THE END OF THIS SAMPLE? YES _____ NO _____

CALCULATIONS

$$V_{m-std} = 17.65 (V_m) \left(\frac{P_{bar} + \Delta H / 13.6}{T_m + 460} \right) = 17.65 () \left(\frac{ + 13.6 }{ } \right)$$

$$= 17.65 () () = \text{_____ FT}^3$$

$$V_{w-std} (H_2O) = \frac{\text{GRAMS COLLECTED}}{21.2 \text{ GRAMS/FT}^3} = \frac{()}{(21.2)} = \text{_____ FT}^3$$

$$\% H_2O = \frac{(V_{w-std}) 100}{((V_{w-std}) + (V_{m-std}))} = \frac{100 ()}{() ()} = \frac{()}{()} = \text{_____ \%}$$

$$\text{MOLECULAR WEIGHT (MW)} = \frac{18 (\% H_2O)}{100} + \frac{\text{DRY MW} (100 - \% H_2O)}{100} = 0.18 () + \frac{() ()}{100}$$

$$\text{VELOCITY (ACTUAL) IN STACK} = 85.48 (C_p) \sqrt{\frac{T_s + 460}{P_s (MW)}} \sqrt{\Delta P} = 85.48 () \sqrt{\frac{()}{() ()}} \sqrt{\Delta P}$$

$$V_s = () \sqrt{\Delta P} = () () \sqrt{\Delta P}$$

$$V_s = () \Delta P = () () = \text{_____ FT/SEC}$$

$$ACFM = (V_s) (60) (CSA) = () (60) () = \text{_____}$$

$$\text{VELOCITY @ Stp } V_{s-std} = V_s (17.65) \left(\frac{P_s}{T_s + 460} \right) = \frac{() (17.65) ()}{()} = \text{_____ FT/SEC}$$

$$SCFM = (V_{s-std}) (CSA) (60) = () () (60) = \text{_____}$$

$$DSCFM = \left(\frac{100 - \% H_2O}{100} \right) (SCFM) = () () = \text{_____}$$

$$\text{NOZZLE VELOCITY @ STD } V_n = \frac{(V_{m-std} + V_{w-std})}{60 (0) A_n} = \frac{()}{60 () () (10^{-4})} = \text{_____ FT/SEC}$$

$$I = \frac{100 V_{n-std}}{V_{s-std}} = \frac{100 ()}{()} = \text{_____ \% Isokinetic}$$

LAB DATA - EVAPORATIONS

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PLANT Hills Bros.SAMPLE LOCATION #23 OutletRUN NO. 2 FORSAMPLING DATE 8/31/88

OPERATING CONDITION

CHAIN-OF-CUSTODY SAMPLE NO.

ACETONE WASHINGS

GROSS 573.9 GMS
 TOTAL SAMPLE TARE - 410.2 GMS
 (A) NET 163.7 GMS
 AMOUNT EVAPORATED (B) 163.7 GMS
 EVAP. BEAKER NO. _____
 GROSS 98.7161 GMS
 TARE - 98.7078 GMS
 (C) NET 0.0023 GMS

ACETONE BLANK

EVAP. BEAKER NO. _____
 GROSS 97.6580 GMS
 TARE - 97.6583 GMS
 NET 0 GMS
 ACETONE BLANK = NET 0 GMS (D)
 TOTAL AMOUNT EVAPORATED 200 GMS (F)

CORRECTED NET (E) = (C) - (B) $\left[\frac{(D)}{(F)} \right]$
 = 0.0023 - 163.7 $\left[\frac{0}{200} \right]$
 = 0.0023 GMS (E) = (C) - B $\left[\frac{(D)}{(F)} \right]$

SCALED UP NET = (E) $\left(\frac{A}{B} \right)$
 = 0.0023 $\left(\frac{163.7}{163.7} \right)$
 = 0.0023 GMS

WET CATCH

GROSS _____ GMS
 TOTAL SAMPLE TARE - _____ GMS
 (A) NET _____ GMS
 AMOUNT EXTRACTED (G) _____ GMS (MLS)
 AMOUNT OF EXC _____ GMS (H)

WATER PHASE
EVAP. BEAKER NO. _____

GROSS _____ GMS
 TARE - _____ GMS
 (J) NET _____ GMS
 WATER BLANK (L) = _____ GMS
 100 GMS

CORRECTED NET (N) = J - (G) $\left(\frac{L}{100} \right)$
 = _____ GMS

SCALED UP NET = (N) $\left(\frac{F}{G} \right)$
 = _____ GMS

EC PHASE
EVAP. BEAKER NO. _____

GROSS _____ GMS
 TARE - _____ GMS
 (K) NET _____ GMS
 E/C BLANK (M) = _____ GMS
 100 HLS

CORRECTED NET (H) = K - (H) $\left(\frac{M}{100} \right)$
 = _____ GMS

SCALED UP NET = (P) $\left(\frac{F}{G} \right)$
 = _____ GMS

Particulates

Nozzle, Probe, and Acetone Washing .0023 grms

Filter .0029 grms

Enter "0" if no Organic or Aqueous Phase

Aqueous Phase 0 grms

Organic Phase 0 grms

Totals

GRAINS/DSCF = 1.985317E-03

POUNDS/HOUR = 7.491164E-02

HIT RETURN TO CONTINUE

PARTICULATE FIELD DATA SHEET

PLANT 21 115 DAYS

DATE 8/31/58

RUN NO. 3

SAMPLE LOCATION *04727*

RAC BOX NO 4

DRY GAS METER NO.

NOZZLE NO. NOZZLE SIZE 7/16 INCHES

PILOT NO 7

2

TIME AT EACH POINT (B)	MINUTES
1	1
2	2
3	3
4	4
5	5
6	6
7	7
8	8
9	9
10	10
11	11
12	12
13	13
14	14
15	15
16	16
17	17
18	18
19	19
20	20
21	21
22	22
23	23
24	24
25	25
26	26
27	27
28	28
29	29
30	30
31	31
32	32
33	33
34	34
35	35
36	36
37	37
38	38
39	39
40	40
41	41
42	42
43	43
44	44
45	45
46	46
47	47
48	48
49	49
50	50
51	51
52	52
53	53
54	54
55	55
56	56
57	57
58	58
59	59
60	60
61	61
62	62
63	63
64	64
65	65
66	66
67	67
68	68
69	69
70	70
71	71
72	72
73	73
74	74
75	75
76	76
77	77
78	78
79	79
80	80
81	81
82	82
83	83
84	84
85	85
86	86
87	87
88	88
89	89
90	90
91	91
92	92
93	93
94	94
95	95
96	96
97	97
98	98
99	99
100	100

DELTA H 200 THERMOCO

FILE NO. 4

AMBIENT PRESSURE (P_{amb}) 29.98 "HG

PROBE OUTLEY
BOY OUTLEY

STATIC PRESSURE (P) -0.13 "H₂O/13.6

"Hg/P, no

Box 1

STACK PRESSURE (P_s) = $P_{\text{hot}} + P_{\text{water}} =$

"NO OPERATING CON

ADDITIONAL REMARKS

DRY BULB 75°F WET BULB 62°F RH 43

PH $\frac{1}{2}H_2O$

[illegible]

* Sum, average or Difference

Pre-Leak Check ☒

Post Leak Check ✓

FYRITE: % OXYGEN 21
% CARBON DIOXIDE 0

PARTICULATE.ATG (August 1988)

stop 18:49:45
Restart 18:59:45

19:15:30 Stop
19:17:30 Reservoir
THREE BRIDGES, NJ

CLIENT: HILLS BROS.

Date: 09/19/88

Time: 10:21 AM

Delta H (IN H2O)	Meter Temp (F)		Stack Temp (F)
	IN	OUT	
2.00	91.00	89.00	1203.00
2.00	93.00	88.00	1226.00
2.00	96.00	88.00	1237.00
1.90	97.00	88.00	1227.00
1.40	98.00	88.00	1206.00
1.05	101.00	88.00	1204.00
1.90	98.00	89.00	1195.00
2.00	102.00	89.00	1219.00
2.00	102.00	89.00	1234.00
1.90	103.00	90.00	1227.00
1.50	102.00	89.00	1189.00
1.05	102.00	89.00	1189.00

AVERAGES

DELTA H = 1.725 IN H2O

METER TEMP. = 127.375 F

TACK TEMP. = 1213 F

CLIENT: HILLS BROS.

Date: 09/19/88

Time: 10:21 AM

AVERAGE VELOCITY PRESSURE

<u>Delta P</u> <u>(IN H2O)</u>	<u>Delta P</u> <u>Square Root</u>
0.17	0.41
0.17	0.41
0.17	0.41
0.16	0.40
0.12	0.35
0.00	0.00
0.16	0.40
0.17	0.41
0.17	0.41
0.16	0.40
0.13	0.36
0.00	0.00

THE AVERAGE SQUARE ROOT OF DELTA P = .3807099

HYDROCARBON SAMPLING DATA

SAMPLE LOCATION

outlet

RUN NO.

3

DATE

8/31/88

HYDROCARBON PUMP NO.

2

TIME	ROTOMETER SETTING	GAS METER TEMP.	VACUUM "HG	SAMPLE RATE L/M
1849	60	80	1	.93
1904	60	80	1	.93
1909	60	80	1	.93
1914	60	80	1	.93
1921	60	80	1	.93
1926	60	80	1	.93
1931	stop	81	1	
1935	start 60	81	1	.93
1940	60	81	1	.93
1945	60	81	1	.93
1950	60	81	1	.93
1955	60	80	1	.93
2000	60	80	1	.93

PRE-LEAK CHECK

POST-LEAK CHECK

PUMP CALIBRATION FLOW RATE		CALIBRATION INSTRUMENT	FYRITE
FLOW RATE LITERS/MIN	ROTAMETER SETTING	SOAP FILM BURET DRY GAS METER OTHER	% OXYGEN % CARBON DIOXIDE
.933	60		

CORRECTING ROTOMETER VOLUME TO DRY STANDARD CONDITIONS

$$\text{EQUATION: } V_{\text{STD}} = V_m \times \frac{P_m}{T_m} \times \frac{T_{\text{STD}}}{P_{\text{STD}}}$$

WHERE:

- V_m = SAMPLE RATE OF ROTOMETER (L/M)
 T_{STD} = $70^{\circ}\text{F} + 460^{\circ}\text{F} = 530^{\circ}\text{F}$
 P_{STD} = 29.92°HG
 P_m = BAROMETRIC PRESSURE DURING SAMPLING ("HG)
 T_m = TEMPERATURE OF GAS STREAM ($+460^{\circ}\text{F}$)

$$V_{\text{STD}} = \quad \times \left(\frac{\quad}{\quad} \right) \times \frac{(530)}{(29.92)} = \quad$$

$$\text{CF} = (V_{\text{STD}} \text{ L/MIN}) (3.53 \times 10^{-2} \text{ CF/L}) (60 \text{ MIN/1 HR}) = (\quad) (3.53 \times 10^{-2}) (60)$$

$$= \quad \text{CFH}$$

18:49:45 stop
 18:59:45 restart
 19:15:30 stop
 19:17:30 start

MOISTURE DETERMINATION

SAMPLE LOCATION outletRUN NO. 3DATE 8/31/88

CHAIN-OF-CUSTODY SAMPLE NO. _____

GRAMS

IMPINGER 1 FINAL WEIGHT 883.1
INITIAL WEIGHT 723.7
INCREASE

IMPINGER 2 FINAL WEIGHT 651.5
INITIAL WEIGHT 630.7
INCREASE

IMPINGER 3 FINAL WEIGHT 487.7
INITIAL WEIGHT 489.5
INCREASE

SILICA GEL FINAL WEIGHT 808.7
INITIAL WEIGHT 797.0
INCREASE

GRAMS

IMPINGER 1 159.7

IMPINGER 2 20.0

IMPINGER 3 .1

SILICA GEL 11.7

TOTAL MASS OF WATER CAUGHT

175.6 GRAMS

CHAIN-OF-CUSTODY SAMPLE NO. _____

FILTER DIAMETER 4 INCHESFILTER TYPE Glass fiber

FILTER: FINAL WEIGHT 0.6146 GMS
INITIAL WEIGHT 0.6134 GMS
INCREASE

0.0012 GRAMS

TOTAL MASS OF PARTICULATE CAUGHT THIS FILTER

IS ICE PRESENT IN THE IMPINGER BATH AT THE END OF THIS SAMPLE? YES _____ NO _____

CALCULATIONS

$$V_{m-std} = 17.65 (V_m) \left(\frac{P_{bar} + \Delta H / 13.6}{T_m + 460} \right) = 17.65 () \left(\frac{+ 13.6}{+ 460} \right)$$

$$= 17.65 () () = \text{_____ FT}^3$$

$$V_{w-std} (H_2O) = \frac{\text{GRAMS COLLECTED}}{21.2 \text{ GRAMS/FT}^3} = \frac{()}{(21.2)} = \text{_____ FT}^3$$

$$\% H_2O = \frac{(V_{w-std}) 100}{((V_{w-std}) + (V_{m-std}))} = \frac{100 ()}{() ()} = \frac{()}{()} = \text{_____ \%}$$

$$\text{MOLECULAR WEIGHT (MW)} = \frac{18 (\% H_2O)}{100} + \frac{\text{DRY MW} (100 - \% H_2O)}{100} = 0.18 () + \frac{() ()}{100}$$

$$\text{VELOCITY (ACTUAL) IN STACK} = 85.48 (C_p) \sqrt{\frac{T_s + 460}{P_s (MW)}} \sqrt{\Delta P} = 85.48 () \sqrt{\frac{()}{() ()}} \sqrt{\Delta P}$$

$$V_s = () \sqrt{\Delta P} = () () \sqrt{\Delta P}$$

$$V_s = () \Delta P = () () = \text{_____ FT/SEC}$$

$$ACFM = (V_s)(60)(CSA) = () (60) () = \text{_____}$$

$$\text{VELOCITY @ Stp } V_{s-std} = V_s (17.65) \left(\frac{P_s}{T_s + 460} \right) = \frac{() (17.65) ()}{()} = \text{_____ FT/SEC}$$

$$SCFM = (V_{s-std})(CSA)(60) = () () (60) = \text{_____}$$

$$DSCFM = \left(\frac{100 - \% H_2O}{100} \right) (SCFM) = () () = \text{_____}$$

$$\text{NOZZLE VELOCITY @ STD } V_n = \frac{(V_{m-std} + V_{w-std})}{60 (8) A_n} = \frac{()}{60 () () (10^{-4})} = \text{_____ FT/SEC}$$

$$I = \frac{100 V_{n-std}}{V_{s-std}} = \frac{100 ()}{()} = \text{_____ \% Isokinetic}$$

LAB DATA - EVAPORATIONS

PLANT Hills Bros.SAMPLE LOCATION #23 OutletRUN NO. 3 FOR _____SAMPLING DATE 8/31/88

OPERATING CONDITION _____

CHAIN-OF-CUSTODY SAMPLE NO. _____

ACETONE WASHINGS

GROSS 577.0 GMS
 TOTAL SAMPLE TARE - 408.7 GMS
 (A) NET 168.3 GMS
 AMOUNT EVAPORATED (B) 168.3 GMS
 EVAP. BEAKER NO. _____
 GROSS 164.3903 GMS
 TARE - 164.3820 GMS
 (C) NET 0.0083 GMS

ACETONE BLANK

EVAP. BEAKER NO. _____
 GROSS 97.6580 GMS
 TARE - 97.6583 GMS
 NET 0 GMS
 ACETONE BLANK = NET 0 GMS (D)
 TOTAL AMOUNT EVAPORATED 200 GMS (F)

$$\begin{aligned} \text{CORRECTED NET (E)} &= (C) - (B) \left[\frac{(D)}{(F)} \right] \\ &= (0.0083) - (168.3) \left[\frac{0}{200} \right] \\ &= 0.0083 \text{ GMS (E)} = (C) - B \left[\frac{(D)}{(F)} \right] \end{aligned}$$

$$\begin{aligned} \text{SCALED UP NET} &= (E) \left(\frac{A}{B} \right) \\ &= 0.0083 \left(\frac{168.3}{168.3} \right) \\ &= 0.0083 \text{ GMS} \end{aligned}$$

WET CATCH

GROSS _____ GMS
 TOTAL SAMPLE TARE - _____ GMS
 (A) NET _____ GMS
 AMOUNT EXTRACTED (G) _____ GMS (HLS)
 AMOUNT OF E/C _____ GMS (H)

WATER PHASE
EVAP. BEAKER NO. _____

GROSS _____ GMS
 TARE - _____ GMS
 (J) NET _____ GMS
 WATER BLANK (L) = _____ GMS
 100 GMS

$$\begin{aligned} \text{CORRECTED NET (N)} &= J - (G)(L) \\ &= \frac{\quad}{100} \\ &= \text{GMS} \end{aligned}$$

$$\begin{aligned} \text{SCALED UP NET} &= (N) \left(\frac{F}{G} \right) \\ &= \frac{\quad}{\quad} \\ &= \text{GMS} \end{aligned}$$

EC PHASE
EVAP. BEAKER NO. _____

GROSS _____ GMS
 TARE - _____ GMS
 (K) NET _____ GMS
 E/C BLANK (M) = _____ GMS
 100 HLS

$$\begin{aligned} \text{CORRECTED NET (M)} &= K - (H)(M) \\ &= \frac{\quad}{100} \\ &= \text{GMS} \end{aligned}$$

$$\begin{aligned} \text{SCALED UP NET} &= (P) \left(\frac{F}{G} \right) \\ &= \frac{\quad}{\quad} \\ &= \text{GMS} \end{aligned}$$

Particulates

Nozzle, Probe, and Acetone Washing .0083 grms

Filter .0012 grms

Enter "0" if no Organic or Aqueous Phase

Aqueous Phase 0 grms

Organic Phase 0 grms

Totals

GRAINS/DSCF = 3.868192E-03

POUNDS/HOUR = .1438865

HIT RETURN TO CONTINUE

CLIENT: HILLS BROS.

Date: 09/19/88

Time: 10:21 AM

ISOKINETIC CALCULATIONS

SAMPLE NO.	1	2	3
DATE	8/31/88	8/31/88	8/31/88
TIME	0833-0937	1642-1745	1849-2005
UNIT SAMPLED	#23 OUTLET	#23 OUTLET	#23 OUTLET
METER VOLUME (VM-STD), SCU-FT	38.11	40.42	37.90
WATER COLLECTED (VW-STD), SCU-FT	8.17	8.46	8.31
MOISTURE (VOL %)	17.66	17.30	17.99
ACTUAL MOLECULAR WEIGHT (MW), LBS/LB-MOLE	26.94	26.98	26.91
ACTUAL VELOCITY IN STACK (VS), FT/SEC	37.45	39.50	39.35
ACTUAL FLOW RATE IN STACK (ACFM)	15875.48	16747.00	16682.61
VELOCITY @ STP (VS-STD), FT/SEC	11.94	12.56	12.48
STACK FLOW RATE @ STP (SCFM)	5061.60	5323.35	5291.38
DRY FLOW RATE (DSCFM)	4167.66	4402.18	4339.71
NOZZLE VELOCITY @ STP (VN-STD), FT/SEC	12.31	13.01	12.30
ISOKINETIC %	103.15	103.58	98.52

CLIENT: HILLS BROS.

Date: 09/19/88

Time: 10:21 AM

THE FOLLOWING WERE PROGRAMMER INPUTS FOR ISOKINETICS

SAMPLE NO.	1	2	3
DATE	8/31/88	8/31/88	8/31/88
TIME	0833-0937	1642-1745	1849-2005
UNIT SAMPLED	#23 OUTLET	#23 OUTLET	#23 OUTLET
ACTUAL NOZZLE DIAMETER (ND), IN	0.44	0.44	0.44
PITOT FACTOR (CF)	0.84	0.84	0.84
TIME @ EACH POINT (MIN)	5.00	5.00	5.00
AMBIENT PRESSURE (PBAR), IN-HG	29.98	29.98	29.98
STACK PRESSURE (PS), IN-HG	-0.11	-0.14	-0.13
METER VOLUME (VM), CU-FT	40.07	42.42	41.89
WATER COLLECTED IMPINGERS, GRMS	172.70	178.70	175.60
CARBON DIOXIDE (CO ₂), %	0.10	0.10	0.10
OXYGEN (O ₂), %	21.10	21.10	21.10
STACK DIAMETER (DIA), IN	36.00	36.00	36.00
STACK CROSS SECTIONAL AREA (CSA), FT ²	7.07	7.07	7.07

Company Name: HILLS BROS. Total Wet Catch(mls) : 44.00
 Location: #23 OUTLET Sample Volume(std. FT3): 2.12
 Unit: Stack Flowrate(DSCFM): 4168.00
 Sample I.D.: RUN 1 Stack % Moisture: 17.60

Contaminants	Name	MW	GC:Liquid Concentration (mg/l)	GC: Gas Concentration (ppmv)
(1)	THC as METHANE	16.05	7.500	134.000
(2)	CARBON MONOXIDE	28.01	0.000	2.200
(3)				
(4)				
(5)				
(6)				
(7)				
(8)				
(9)				
(10)				

Concentrations and Emissions

Contaminants	Name	LB/HR	PPMV(WET)	PPMV(DRY)
(1)	THC as METHANE	1.485	117.177	142.205
(2)	CARBON MONOXIDE	0.040	1.813	2.200
(3)	0.00	0.000	ERR	ERR
(4)	0.00	0.000	ERR	ERR
(5)	0.00	0.000	ERR	ERR
(6)	0.00	0.000	ERR	ERR
(7)	0.00	0.000	ERR	ERR
(8)	0.00	0.000	ERR	ERR
(9)	0.00	0.000	ERR	ERR
(10)	0.00	0.000	ERR	ERR

This Program Uses the Following Equations for Each Contaminant Where:

A = Total Wet Catch(mls) E = GC: Liquid Concentration (mg/l)
 B = Sample Volume (std. FT3) F = GC: Gas Concentration (dry ppmv)
 C = Stack Moisture (%) G = Contaminant's Molecular Weight
 D = Stack Flowrate (DSCFM)

For The Impinger Contents:

$$(H1) = \text{dry ppmv} = (0.846 \times (A) \times (E)) / ((G) \times (B))$$

$$(J1) = \text{wet ppmv} = (\text{dry ppmv}) \times (100 - (C)) / 100$$

$$(K1) = \text{pounds/hour} = 0.000000133 \times (A) \times (E) \times (D) / (B)$$

For the Gas Bag Contents:

$$(H2) = \text{dry ppmv} = (F)$$

$$(J2) = \text{wet ppmv} = (\text{dry ppmv}) \times (100 - (C)) / 100$$

$$(K2) = \text{pounds/hour} = 0.000000156 \times (\text{dry ppmv}) \times (D) \times (G)$$

Concentrations and Emissions:

$$\text{Total dry ppmv} = (H1) + (H2)$$

$$\text{Total wet ppmv} = (J1) + (J2)$$

$$\text{Total pounds/hour} = (K1) + (K2)$$

N.J. Method #3 Gas Bag and Impinger Contents Data Sheet

Company Name: HILLS BROS.
 Location: #23 OUTLET
 Unit:
 Sample I.D.: RUN 2

Total Wet Catch(mls) : 44.00
 Sample Volume(std. FT3): 2.11
 Stack Flowrate(DSCFM): 4402.00
 Stack % Moisture: 17.30

Contaminants	Name	MW	GC: Liquid Concentration (mg/l)	GC: Gas Concentration (ppmv)
(1)	THC as METHANE	16.05	7.500	90.000
(2)	CARBON MONOXIDE	28.01	0.000	1.300
(3)				
(4)				
(5)				
(6)				
(7)				
(8)				
(9)				
(10)				

Concentrations and Emissions				
Contaminants	Name	LB/HR	PPMV (WET)	PPMV (DRY)
(1)	THC as METHANE	1.083	81.215	98.205
(2)	CARBON MONOXIDE	0.025	1.075	1.300
(3)	0.00	0.000	ERR	ERR
(4)	0.00	0.000	ERR	ERR
(5)	0.00	0.000	ERR	ERR
(6)	0.00	0.000	ERR	ERR
(7)	0.00	0.000	ERR	ERR
(8)	0.00	0.000	ERR	ERR
(9)	0.00	0.000	ERR	ERR
(10)	0.00	0.000	ERR	ERR

This Program Uses the Following Equations for Each Contaminant Where:

A = Total Wet Catch(mls)
 B = Sample Volume (std. FT3)
 C = Stack Moisture (%)
 D = Stack Flowrate (DSCFM)

E = GC: Liquid Concentration (mg/l)
 F = GC: Gas Concentration (dry ppmv)
 G = Contaminant's Molecular Weight

For The Impinger Contents:

$$(H1) = \text{dry ppmv} = (0.846 \times (A) \times (E)) / ((G) \times (B))$$

$$(J1) = \text{wet ppmv} = (\text{dry ppmv}) \times (100 - (C)) / 100$$

$$(K1) = \text{pounds/hour} = 0.000000133 \times (A) \times (E) \times (D) / (B)$$

For the Gas Bag Contents:

$$(H2) = \text{dry ppmv} = (F)$$

$$(J2) = \text{wet ppmv} = (\text{dry ppmv}) \times (100 - (C)) / 100$$

$$(K2) = \text{pounds/hour} = 0.000000156 \times (\text{dry ppmv}) \times (D) \times (G)$$

Concentrations and Emissions:

$$\text{Total dry ppmv} = (H1) + (H2)$$

$$\text{Total wet ppmv} = (J1) + (J2)$$

$$\text{Total pounds/hour} = (K1) + (K2)$$

N.J. Method #3 Gas Bag and Impinger Contents Data Sheet

Company Name: HILLS BROS. Total Wet Catch(mls) : 44.00
 Location: #23 OUTLET Sample Volume(std. FT3): 2.12
 Unit: Stack Flowrate(DSCFM): 4340.00
 Sample I.D.: RUN 3 Stack % Moisture: 18.00

Contaminants	Name	MW	GC: Liquid Concentration (mg/l)	GC: Gas Concentration (ppmv)
(1)	THC as METHANE	16.05	7.500	58.000
(2)	CARBON MONOXIDE	28.01	0.000	1.300
(3)				
(4)				
(5)				
(6)				
(7)				
(8)				
(9)				
(10)				

Concentrations and Emissions				
Contaminants	Name	LB/HR	PPMV (WET)	PPMV (DRY)
(1)	THC as METHANE	0.720	54.288	66.205
(2)	CARBON MONOXIDE	0.025	1.066	1.300
(3)	0.00	0.000	ERR	ERR
(4)	0.00	0.000	ERR	ERR
(5)	0.00	0.000	ERR	ERR
(6)	0.00	0.000	ERR	ERR
(7)	0.00	0.000	ERR	ERR
(8)	0.00	0.000	ERR	ERR
(9)	0.00	0.000	ERR	ERR
(10)	0.00	0.000	ERR	ERR

This Program Uses the Following Equations for Each Contaminant Where:

A = Total Wet Catch(mls) E = GC: Liquid Concentration (mg/l)
 B = Sample Volume (std. FT3) F = GC: Gas Concentration (dry ppmv)
 C = Stack Moisture (%) G = Contaminant's Molecular Weight
 D = Stack Flowrate (DSCFM)

For The Impinger Contents:

$$(H1) = \text{dry ppmv} = (0.846 \times (A) \times (E)) / ((G) \times (B))$$

$$(J1) = \text{wet ppmv} = (\text{dry ppmv}) \times (100 - (C)) / 100$$

$$(K1) = \text{pounds/hour} = 0.000000133 \times (A) \times (E) \times (D) / (B)$$

For the Gas Bag Contents:

$$(H2) = \text{dry ppmv} = (F)$$

$$(J2) = \text{wet ppmv} = (\text{dry ppmv}) \times (100 - (C)) / 100$$

$$(K2) = \text{pounds/hour} = 0.000000156 \times (\text{dry ppmv}) \times (D) \times (G)$$

Concentrations and Emissions:

$$\text{Total dry ppmv} = (H1) + (H2)$$

$$\text{Total wet ppmv} = (J1) + (J2)$$

$$\text{Total pounds/hour} = (K1) + (K2)$$

N.J. Method #3 Gas Bag and Impinger Contents Data Sheet

Company Name: HILLS BROS.
 Location: #23 OUTLET
 Unit: _____
 Sample I.D.: RUN 1

Total Wet Catch(mls) : 44.00
 Sample Volume(std. FT3): 2.1
 Stack Flowrate(DSCFM): 4168.00
 Stack % Moisture: 17.60

Contaminants	Name	MW	GC: Liquid Concentration (mg/l)	GC: Gas Concentration (ppmv)
(1)	THC as METHANE	16.05	0.000	134.000
(2)				
(3)				
(4)				
(5)				
(6)				
(7)				
(8)				
(9)				
(10)				

Concentrations and Emissions				
Contaminants	Name	LB/HR	PPMV (WET)	PPMV (DRY)
(1)	THC as METHANE	1.398	110.416	134.000
(2)	0.00	0.000	ERR	ERR
(3)	0.00	0.000	ERR	ERR
(4)	0.00	0.000	ERR	ERR
(5)	0.00	0.000	ERR	ERR
(6)	0.00	0.000	ERR	ERR
(7)	0.00	0.000	ERR	ERR
(8)	0.00	0.000	ERR	ERR
(9)	0.00	0.000	ERR	ERR
(10)	0.00	0.000	ERR	ERR

This Program Uses the Following Equations for Each Contaminant Where:

A = Total Wet Catch(mls)
 B = Sample Volume (std. FT3)
 C = Stack Moisture (%)
 D = Stack Flowrate (DSCFM)

E = GC: Liquid Concentration (mg/l)
 F = GC: Gas Concentration (dry ppmv)
 G = Contaminant's Molecular Weight

For The Impinger Contents:

$$(H1) = \text{dry ppmv} = (0.846 \times (A) \times (E)) / ((G) \times (B))$$

$$(J1) = \text{wet ppmv} = (\text{dry ppmv}) \times (100 - (C)) / 100$$

$$(K1) = \text{pounds/hour} = 0.000000133 \times (A) \times (E) \times (D) / (B)$$

For the Gas Bag Contents:

$$(H2) = \text{dry ppmv} = (F)$$

$$(J2) = \text{wet ppmv} = (\text{dry ppmv}) \times (100 - (C)) / 100$$

$$(K2) = \text{pounds/hour} = 0.000000156 \times (\text{dry ppmv}) \times (D) \times (G)$$

Concentrations and Emissions:

$$\text{Total dry ppmv} = (H1) + (H2)$$

$$\text{Total wet ppmv} = (J1) + (J2)$$

$$\text{Total pounds/hour} = (K1) + (K2)$$

N.J. Method #3 Gas Bag and Impinger Contents Data Sheet

Company Name: HILLS BROS.	Total Wet Catch(mls) :	44.00
Location: #23 OUTLET	Sample Volume(std. FT3):	2.12
Unit: _____	Stack Flowrate(DSCFM):	4402.00
Sample I.D.: RUN 2	Stack % Moisture:	17.30

Contaminants	Name	MW	GC: Liquid Concentration (mg/l)	GC: Gas Concentration (ppmv)
(1)	THC as METHANE	16.05	0.000	90.000
(2)				
(3)				
(4)				
(5)				
(6)				
(7)				
(8)				
(9)				
(10)				

Concentrations and Emissions

Contaminants	Name	LB/HR	PPMV(WET)	PPMV(DRY)
(1)	THC as METHANE	0.992	74.430	90.000
(2)	0.00	0.000	ERR	ERR
(3)	0.00	0.000	ERR	ERR
(4)	0.00	0.000	ERR	ERR
(5)	0.00	0.000	ERR	ERR
(6)	0.00	0.000	ERR	ERR
(7)	0.00	0.000	ERR	ERR
(8)	0.00	0.000	ERR	ERR
(9)	0.00	0.000	ERR	ERR
(10)	0.00	0.000	ERR	ERR

This Program Uses the Following Equations for Each Contaminant Where:

A = Total Wet Catch(mls)	E = GC: Liquid Concentration (mg/l)
B = Sample Volume (std. FT3)	F = GC: Gas Concentration (dry ppmv)
C = Stack Moisture (%)	G = Contaminant's Molecular Weight
D = Stack Flowrate (DSCFM)	

For The Impinger Contents:

(H1) = dry ppmv = $(0.846 \times (A) \times (E)) / ((G) \times (B))$
 (J1) = wet ppmv = (dry ppmv) $\times (100 - (C)) / 100$
 (K1) = pounds/hour = $0.000000133 \times (A) \times (E) \times (D) / (B)$

For the Gas Bag Contents:

(H2) = dry ppmv = (F)
 (J2) = wet ppmv = (dry ppmv) $\times (100 - (C)) / 100$
 (K2) = pounds/hour = $0.000000156 \times (\text{dry ppmv}) \times (D) \times (G)$

Concentrations and Emissions:

Total dry ppmv = (H1) + (H2)
 Total wet ppmv = (J1) + (J2)
 Total pounds/hour = (K1) + (K2)

N.J. Method #3 Gas Bag and Impinger Contents Data Sheet

Company Name: HILLS BROS. Total Wet Catch(mls) : 44.00
 Location: #23 OUTLET Sample Volume(std. FT3): 2.12
 Unit: _____ Stack Flowrate(DSCFM): 4340.00
 Sample I.D.: RUN 3 Stack % Moisture: 18.00

Contaminants	Name	MW	GC: Liquid Concentration (mg/l)	GC: Gas Concentration (ppmv)
(1)	THC as METHANE	16.05	0.000	58.000
(2)				
(3)				
(4)				
(5)				
(6)				
(7)				
(8)				
(9)				
(10)				

Concentrations and Emissions

Contaminants	Name	LB/HR	PPMV(WET)	PPMV(DRY)
(1)	THC as METHANE	0.630	47.560	58.000
(2)	0.00	0.000	ERR	ERR
(3)	0.00	0.000	ERR	ERR
(4)	0.00	0.000	ERR	ERR
(5)	0.00	0.000	ERR	ERR
(6)	0.00	0.000	ERR	ERR
(7)	0.00	0.000	ERR	ERR
(8)	0.00	0.000	ERR	ERR
(9)	0.00	0.000	ERR	ERR
(10)	0.00	0.000	ERR	ERR

This Program Uses the Following Equations for Each Contaminant Where:

A = Total Wet Catch(mls) E = GC: Liquid Concentration (mg/l)
 B = Sample Volume (std. FT3) F = GC: Gas Concentration (dry ppmv)
 C = Stack Moisture (%) G = Contaminant's Molecular Weight
 D = Stack Flowrate (DSCFM)

For The Impinger Contents:

$$(H1) = \text{dry ppmv} = (0.846 \times (A) \times (E)) / ((G) \times (B))$$

$$(J1) = \text{wet ppmv} = (\text{dry ppmv}) \times (100 - (C)) / 100$$

$$(K1) = \text{pounds/hour} = 0.000000133 \times (A) \times (E) \times (D) / (B)$$

For the Gas Bag Contents:

$$(H2) = \text{dry ppmv} = (F)$$

$$(J2) = \text{wet ppmv} = (\text{dry ppmv}) \times (100 - (C)) / 100$$

$$(K2) = \text{pounds/hour} = 0.000000156 \times (\text{dry ppmv}) \times (D) \times (G)$$

Concentrations and Emissions:

$$\text{Total dry ppmv} = (H1) + (H2)$$

$$\text{Total wet ppmv} = (J1) + (J2)$$

$$\text{Total pounds/hour} = (K1) + (K2)$$

Sample: Hills Brothers Plant, Afterburner Inlet and Outlet -
Tested 8-31-88

Method: Volatile Organic Analysis - FID
all units are mg/l*

<u>RECON</u> <u>ID</u>	<u>Run</u> <u>No.</u>	<u>Sample</u> <u>Location</u>	<u>Total</u> <u>Hydrocarbons</u> <u>as Methane</u>
12417	1	Inlet	220
12418	2	Inlet	620
12419	3	Inlet	280
12420	1	Outlet	ND
12421	2	Outlet	ND
12422	3	Outlet	ND

Detection Limit 7.5

ND = none detected, less than the value shown

< = less than the value shown

* = total volume of 44ml

Samples from this project will be retained for sixty days from the date of this report unless otherwise directed.

RECON SYSTEMS, INC.
ROUTE 202N, BOX 460, THREE BRIDGES, NJ 08887
201-782-5900

101

CHAIN-OF-CUSTODY/REQUEST FOR ANALYSIS/DOT SHIPPING PAPER

(Use one sample) PROJECT MANAGER PFM
SAMPLE NO 12417-12419 ANALYTICAL RESULTS TO BE REPORTED TO: PAT
SAMPLE LOCATION After burner Inlet RECON JOB NO. 0654
SAMPLE DESCRIPT. Impinger catch SAMPLING DATE/TIME 8/31/88 0830 BY: PFM/AWM

Relinquished By Person/Organ. (Signature)	Received By Person/Organ./ Date/Time (Signature)	Container Description and Preservative	Analysis Requested	Analysis Performed By Person/Lab	Date/Time Analysis Performed	Results
<u>EM/Rec</u>	<u>ALH/FEL</u> <u>9/4/88</u> <u>0932</u>	<u>B 12417</u> <u>Run 1</u>	<u>Total Hydrocarbons</u> <u>as Methane,</u> <u>EQ</u>	<u>R/MS</u>	<u>8-7</u>	
		<u>B 12418</u> <u>Run 2</u>	<u>Total Hydrocarbons</u> <u>as Methane,</u> <u>EQ</u>	<u>R/MS</u>	<u>8-7</u>	
		<u>B 12419</u> <u>Run 3</u>	<u>Total Hydrocarbons</u> <u>as Methane,</u> <u>EQ</u>	<u>R/MS</u>	<u>8-7</u>	

MAKE ADDITIONAL COMMENTS/NOTES

RUSH ☒ YES ☐ NO
EMERGENCY ☐ YES ☒ NO

COMPLIANCE OR TIER II ☒ COMPLIANCE

IF HAZARDOUS MATERIALS HAVE BEEN DETERMINED HAZARDOUS, PLEASE INCLUDE SHIPPING NAME, HAZARD CLASS, AND IDENTIFICATION NUMBER

COPIES OF THIS FORM MUST BE ATTACHED TO EACH LABORATORY REPORT. DOT 37A (CPB) (July 11, 1988) 37A (CPB)

CHAIN-OF-CUSTODY/REQUEST FOR ANALYSIS/DOT SHIPPING PAPER

(Use one sample)

PROJECT MANAGER PFM

SAMPLE NO. 12420-12422

ANALYTICAL RESULTS TO BE REPORTED TO: DAT

SAMPLE LOCATION After burner Outlet RECON JOB NO. 0654

SAMPLE DESCIP. Impinger catch SAMPLING DATE/TIME 8/31/88 0830 BY: PFM/AWM

Relinquished By Person/Organ. Signature	Received By Person/Organ./ Date/Time (Signature)	Container Description and Preservative	Analysis Requested	Analysis Performed By Person/Lab	Date/Time Analysis Performed	Results
<u>FM/Rec</u>	<u>ALH/FEL</u> <u>9/6/88</u> <u>0935</u>	<u>B 12420</u> <u>RUH 1</u>	<u>Total Hydrocarbons</u> <u>as Methane,</u> <u>DO</u>	<u>RNS</u>	<u>8-7</u>	
		<u>B 12421</u> <u>RUH 2</u>	<u>Total Hydrocarbons</u> <u>as Methane,</u> <u>DO</u>	<u>RNS/R</u>	<u>8-7</u>	
		<u>B 12422</u> <u>RUH 3</u>	<u>Total Hydrocarbons</u> <u>as Methane,</u> <u>DO</u>	<u>RNS/R</u>	<u>8-7</u>	

MAKE ADDITIONAL COMMENTS/NOTES

RUSH

YES ☒ NO ☐

EMERGENCY

YES ☐ NO ☒

COMPLIANCE OR TIER II

YES ☒ NO ☐

SAMPLES HAVE BEEN DETERMINED HAZARDOUS. PLEASE INCLUDE SHIPPING NAME, HAZARD CLASS, AND IDENTIFICATION NUMBER.

Linear Regression Calculations
for Gas Chromatographic Analysis - Impingers

103

RECON SYSTEMS INC
THREE BRIDGES, NJ

STANDARDS		UNKNOWNNS						
Conc. (mg/L)	Area Counts	Sample ID	Sample Number	Sample Area Counts	Dil. Factor	Dil. Samp. Conc. (mg/L)	Actual Conc. (mg/L)	
0	5543	Outlet-1	12420	5179	1.00	N/A	ND<7.5	
70.15	23470	Outlet-2	12421	4794	1.00	N/A	ND<7.5	
1169	349417	Outlet-3	12422	4691	1.00	N/A	ND<7.5	
		Inlet-1	12417	69004	1.00	219.2	219	
		Inlet-2	12418	187981	1.00	622.3	622	
		Inlet-3	12419	85664	1.00	275.7	276	

Method Detection Limit - 7.5 mg/L

COEFF. OF DETERMIN.
0.9999555

COEFF. OF CORRELATION
0.9999777

STD ERROR OF ESTIMATE
1.825E+03

Client: Ambient Engineering
Job Number: 0654
Hills Bros. Plant
Compound: Total HxCx (as Methane)
Sample Location: Afterburner (In & Out)
Sample Date: 8-31-88

Report Date: 07-Sep-88

Samples Run: 6

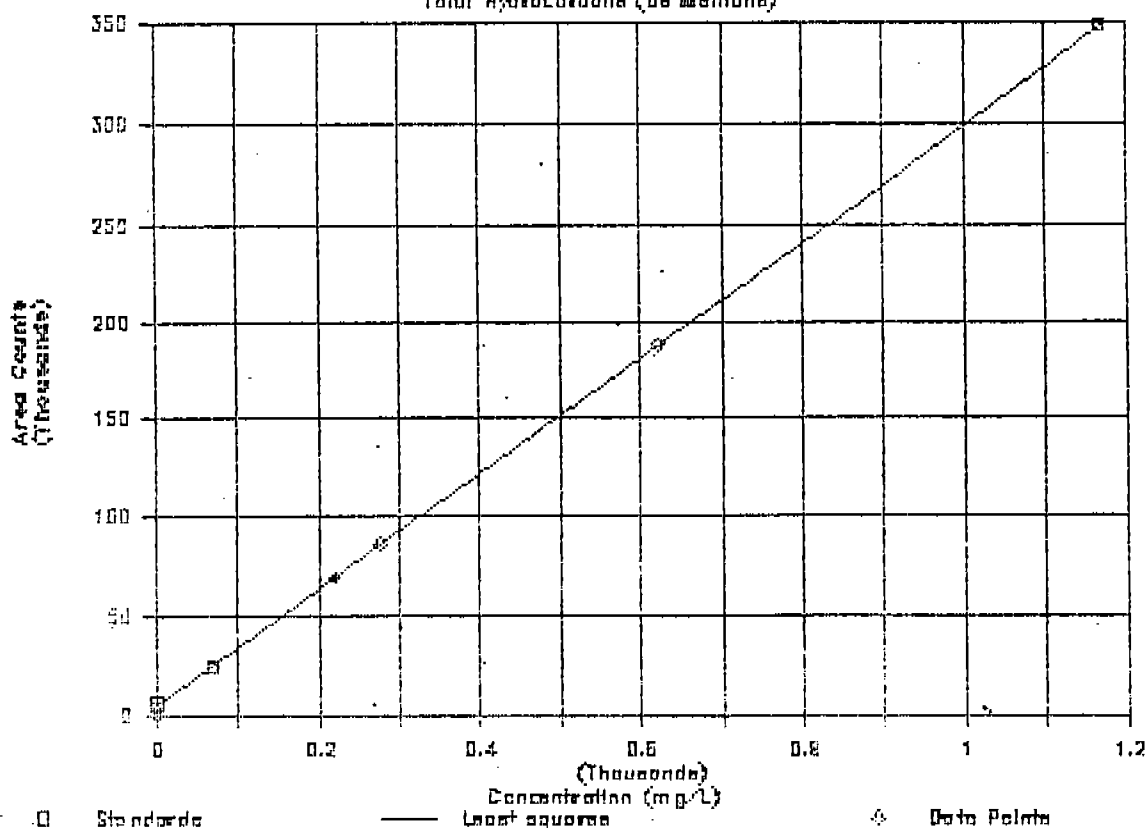
Analyst: RNS

Reference: RNS#2, p.82

2uL inj. of samples and standards.

Total volume of 44 mL.

Gas Chromatographic Analysis
Total Hydrocarbons (as Methane)



PROJECT Ambient Engineering - R#0654 9-7-88

Continued From Page _____

Total Hydrocarbons (Impingers only)
(as Methane)

Analytical Conditions

Tracor 550 - GC/FID

H₂ - 30 psi; Air - 1.0 rate

He carrier - 5.5 rate

inject - 190°C detector - 260°C

isothermal oven - 185°C

col. - 6' x 1/8" IS Glass - empty (glass wool plug)

Nelson Analytical Data Handling

2ul, replicate injections of standards & samples

Att. - 10'

Standardsconc. - as CH₄ (mg/L)50 ~~ul~~ul. Isobutyl Alcohol in 25 ml H₂O: ~~70.15~~ 11693ul Isobutyl Alcohol in 25 ml H₂O: 70.15 - ~~1169~~0.3 ul TBA in 25 ml H₂O: 7.02 - 100 10W -300ul Isobutyl Alcohol in 25ml H₂O: ~~70.15~~ 7015 (if needed)1mg TBA = .728 mg CH₄ - (p. 4 - "Resp. Factors")

Continued on Page

Read and Understood By

Signed

Date

Signed

Date

9-13-88

Interface 11 0-11 Min Scale: 50 Mv
BLANK DIST Processed: 09-07-1988 12:53:03, segment 1, cycle 1
Error, duplicate file name = E:ANB91.PTS
RAW DATA SAVED IN FILE E:ANB91.PTS

***** PRELIMINARY REPORT *****

* Sample Name: BLANK DISTILLED WATER 2uL Operator Initials: RNS
* Date: 09-07-1988 12:53:11 Method: FIDSCAN DATA FILE: E:ANB91.PTS
* Interface: 1 Cycles: 1 Channel#: 0 Vial#: N.A.
* Starting Peak Width: 5 Threshold: 1
* Instrument Type: TRACOR MODEL 550 Column Type: 6' X 1/4" GLASS
* Solvent Description: EMPTY - (GLASS WOOL PLUGS)
* Operating Conditions: ISOTHERMAL OVEN 185-C, INJ. PORT 190-C, DET. 260-C
* Detector 0: FID Detector 1: NONE
* Misc. Information: He carr. 5.5roto, 2uL repl. inj.

START TIME= 10.367 START HEIGHT= 8182
STOP TIME= 9.983 STOP HEIGHT= 8129
AREA = 5541
START TIME= 8.033 START HEIGHT= 8129
STOP TIME= 7.683 STOP HEIGHT= 8202
EA = 5544
START TIME= 6.250 START HEIGHT= 8098
STOP TIME= 5.733 STOP HEIGHT= 7847
AREA = 5914
START TIME= 4.550 START HEIGHT= 7934
STOP TIME= 4.133 STOP HEIGHT= 7998
AREA = 2845
START TIME= 3.033 START HEIGHT= 8192
STOP TIME= 2.533 STOP HEIGHT= 8305
AREA = 4643

106

Plot of data file: E:ANB91.PTS

Date: 09-07-1988 Time: 13:21:45

Sample Name: BLANK DISTILLED S

Start Time= 0.02 Stop Time= 11.00Min. Scale= 7752Max. Scale= 19522

E 19

E 18

AREA= 4643

AREA= 2845

AREA= 5914

AREA= 5544

AREA= 5541

Interface 1] 0-11 Min Scale: 50 Mv
S#12420 0 Processed: 09-07-1988 13:15:08, segment 1, cycle 3
RAW DATA SAVED IN FILE E:AMB93.PTS

***** AREA PERCENT REPORT *****

* Sample Name: S#12420 OUTLET RUN #1 - IMPINGERS

Operator Initials: RNS

DATA FILE: E:AMB93.PTS

Channel#: 0 Vial#: N.A.

* Date: 09-07-1988 13:15:14 Method: FIDSCAN

* Interface: 1 Cycle#: 3

* Starting Peak Width: 5 Threshold: 1

* Instrument Type: TRACOR MODEL 550

Solvent Description: EMPTY - (GLASS WOOL PLUGS)

* Operating Conditions: ISOTHERMAL OVEN 185-C, INJ. PORT 190-C, DET. 260-C

* Detector 0: FID

* Misc. Information: He carr. 5.5roto, 2uL repl. inj.

Starting Delay: 0.00 Ending Retention Time: 11.00

Pk No.	Ret Time	Peak Area	Area %	Peak Ht.	Normalized %	Area/Height
--------	----------	-----------	--------	----------	--------------	-------------

Total Area:

0

Area Reject: %1000000000

One sample per

1,000 sec.

START TIME= 10.133 START HEIGHT= 8502
 TOP TIME= 9.433 STOP HEIGHT= 8314
 AREA = 6945
 START TIME= 8.533 START HEIGHT= 7994
 STOP TIME= 8.067 STOP HEIGHT= 7903
 AREA = 5243
 START TIME= 8.067 START HEIGHT= 7903
 STOP TIME= 7.650 STOP HEIGHT= 8029
 AREA = 3136
 START TIME= 6.383 START HEIGHT= 8097
 STOP TIME= 6.000 STOP HEIGHT= 8178
 AREA = 998
 START TIME= 4.717 START HEIGHT= 8061
 STOP TIME= 4.367 STOP HEIGHT= 7943
 AREA = 5114
 START TIME= 3.533 START HEIGHT= 7756
 STOP TIME= 3.000 STOP HEIGHT= 7710
 AREA = 3979
 START TIME= 1.883 START HEIGHT= 7959
 STOP TIME= 1.417 STOP HEIGHT= 7964
 AREA = 8439

Plot of data file: E:AMB93.PTS

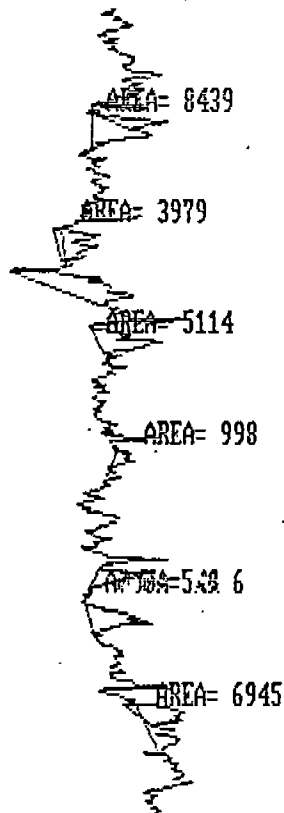
Date: 09-07-1988 Time: 13:42:20

Sample Name: S#12420 OUTLET 5

Start Time= 0.02 Stop Time= 11.00Min. Scale= 7205Max. Scale= 14570

E 19

E 18



[Interface 1] 0-11 Min Scale: 50 Mv
S#12421 0 Processed: 09-07-1988 13:33:48, segment 2, cycle 4
RAW DATA SAVED IN FILE E:AMB94.PTS

***** AREA PERCENT REPORT *****

* Sample Name: S#12421 OUTLET RUN #2 - IMPINGERS *****

Operator Initials: RNS

* Date: 09-07-1988 13:33:55 Method: FIDSCAN

DATA FILE: E:AMB94.PTS

* Interface: 1

Cycle#: 4

Channel#: 0

Vial#: N.A.

* Starting Peak Width: 5

Threshold: 1

* Instrument Type: TRACOR MODEL 550 *****

Solvent Description: EMPTY - (GLASS WOOL PLUGS)

Column Type: 6' X 1/4" GLASS

* Operating Conditions: ISOTHERMAL OVEN 185-C, INJ. PORT 190-C, DET. 260-C

* Detector 0: FID

Detector 1: NONE

* Misc. Information: He carr. 5.5scro, 2uL repl. inj.

Starting Delay: 0.00

Ending Retention Time: 11.00

Pk No.	Ret Time	Peak		Area		Normalized		Area/ Height
		Area	B	%	L	%	Ht.	

Total Area:

0

Area Reject: %1000000000

One sample per

1.000 sec

Areas, times, and heights stored in: E:AMB94.ATB

DATA FILE E:AMB94.HDR TAKEN 09-07-1988 13:33:55

NEW PEAK WIDTH = 10

START TIME= 10.083 START HEIGHT= 8281

STOP TIME= 9.633 STOP HEIGHT= 8137

AREA = 5331

START TIME= 8.067 START HEIGHT= 8242

STOP TIME= 7.667 STOP HEIGHT= 8316

AREA = 4256

START TIME= 6.350 START HEIGHT= 8353

STOP TIME= 5.517 STOP HEIGHT= 8326

AREA = 6818

START TIME= 1.133 START HEIGHT= 8196

STOP TIME= 0.833 STOP HEIGHT= 8099

AREA = 2913

Plot of data file: E:AMB94.PTS

Date: 09-07-1988 Time: 13:39:24

Sample Name: S#12421 OUTLET 5

Start Time= 0.02 Stop Time= 11.00Min. Scale= 7616Max. Scale= 15096

E 19

E 18

AREA= 2913

AREA= 6818

AREA= 4256

AREA= 5331

DATA FILE E:AMB93.HDR TAKEN 09-07-1988 13:15:14

NEW PEAK WIDTH = 10

Check Flame



[Interface 1] 0-11 Min Scale: 50 Mv
S#12423 0 Processed: 09-07-1988 14:14:41, segment 1, cycle 5
RAW DATA SAVED IN FILE E:AMB95.PTS

***** AREA PERCENT REPORT *****

* Sample Name: S#12423 OUTLET RUN #3 - IMPINGERS
* Date: 09-07-1988 14:14:47 Method: FIDSCAN
* Interface: 1
* Starting Peak Width: 5 Threshold: 1
* Operator Initials: RNS
* Data File: E:AMB95.PTS
* Channel#: 0 Vial#: N.A.
* Instrument Type: TRACOR MODEL 550 Column Type: 6' X 1/4" GLASS
* Solvent Description: EMPTY - (GLASS WOOL PLUGS)
* Operating Conditions: ISOTHERMAL OVEN 185-C, INJ. PORT 190-C, DET. 260-C
* Detector 0: FID Detector 1: NONE
* Misc. Information: He carr. 5.5roto, 2uL repl. inj.
* Starting Delay: 0.00 Ending Retention Time: 11.00

Pk No.	Ret Time	Peak	Area	%	B	Peak	Normalized	Area/
		Area			L	Ht.	%	Height

Total Area: 0 Area Reject: %1000000000 One sample per 1.000 sec. 111 111

TA FILE E:AMB95.HDR TAKEN 09-07-1988 14:14:47
NEW PEAK WIDTH = 10

START TIME= 8.650 START HEIGHT= 7645
STOP TIME= 7.917 STOP HEIGHT= 7622

~~AREA = 11570~~

START TIME= 6.700 START HEIGHT= 8047
STOP TIME= 6.267 STOP HEIGHT= 7833

AREA = 3567

START TIME= 5.633 START HEIGHT= 7819
STOP TIME= 5.067 STOP HEIGHT= 7726

AREA = 7221

START TIME= 4.067 START HEIGHT= 7589
STOP TIME= 3.600 STOP HEIGHT= 7673

AREA = 5959

START TIME= 2.033 START HEIGHT= 8037
STOP TIME= 1.550 STOP HEIGHT= 7882

AREA = 2018

Plot of data file: E:AMB95.PTS

Date: 09-07-1988 Time: 16:24:57

Sample Name: S#12425 OUTLET 5

Start Time= 0.02 Stop Time= 11.00Min. Scale= 7327Max. Scale= 27537

E 19

E 10

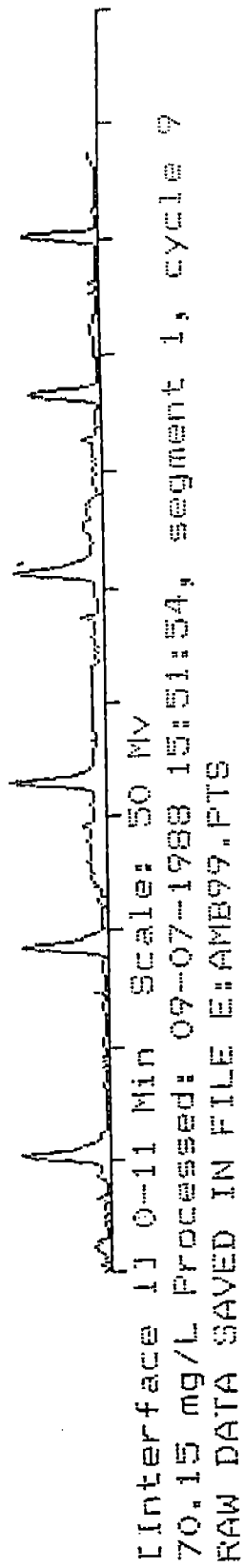
AREA= 2018

AREA= 5959

AREA= 7221

AREA= 3567

AREA= 11570



***** AREA PERCENT REPORT *****

* Sample Name: 70.15 mg/L as Methane 2uL Pre - Cal.
* Date: 09-07-1988 15:52:02 Method: FIDSCAN
* Interfacing: 1
* Starting Peak Width: 5 Threshold: 1
* *****
* Instrument Type: TRACOR MODEL 550
* Solvent Description: EMPTY - (GLASS WOOL PLUGS)
* Operating Conditions: ISOTHERMAL OVEN 185-C, INJ. PORT 190-C, DET. 260-C
* Detector 0: FID
* Misc. Information: He carr. 5.5roto, 2uL repl. inj.
* *****
Starting Delay: 0.00 Ending Retention Time: 11.00

Pk No.	Ret Time	Peak		Area		Normalized		Area/ Height	
		Area	%	B	L	Peak	Ht.	%	Height

DATA FILE E:AMB99.HDR TAKEN 09-07-1988 15:52:02
NEW PEAK WIDTH = 10

START TIME= 9.400 START HEIGHT= 10996
STOP TIME= 8.850 STOP HEIGHT= 10959

AREA = 22277

START TIME= 7.783 START HEIGHT= 11056
STOP TIME= 7.567 STOP HEIGHT= 11128

AREA = 19354

START TIME= 6.600 START HEIGHT= 11712
STOP TIME= 5.983 STOP HEIGHT= 11462

AREA = 25020

START TIME= 4.617 START HEIGHT= 11596
STOP TIME= 4.200 STOP HEIGHT= 11618

AREA = 22605

START TIME= 3.017 START HEIGHT= 11131
STOP TIME= 2.617 STOP HEIGHT= 11062

AREA = 25862

START TIME= 1.250 START HEIGHT= 11338
STOP TIME= 0.767 STOP HEIGHT= 11097

AREA = 31413

START TIME= 1.233 START HEIGHT= 11479
STOP TIME= 0.933 STOP HEIGHT= 11587

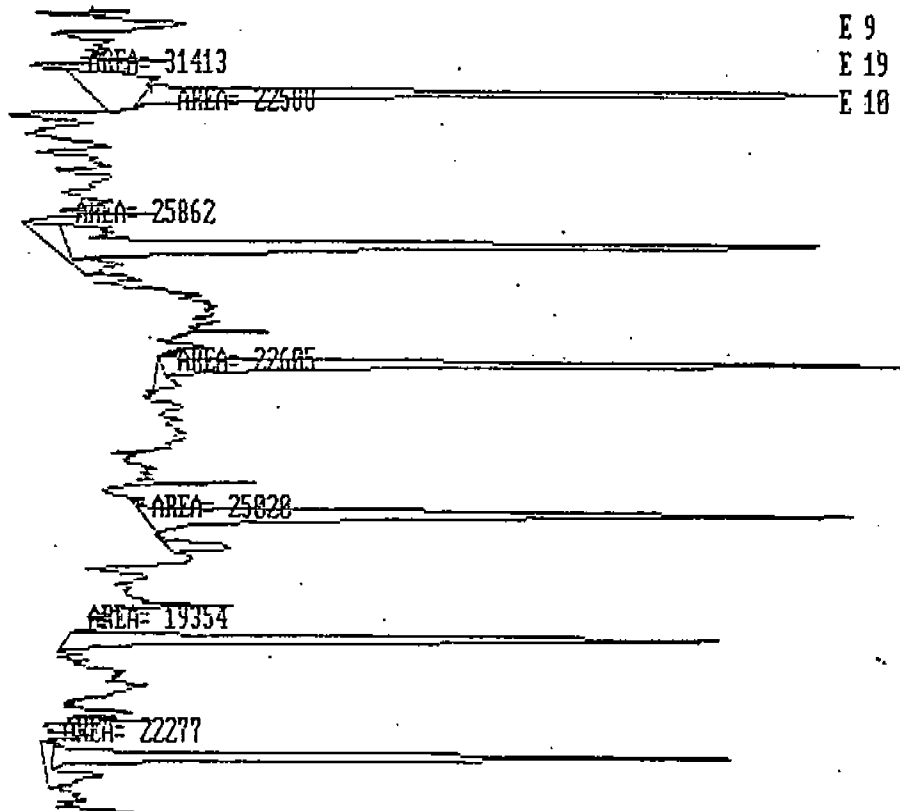
AREA = 22588

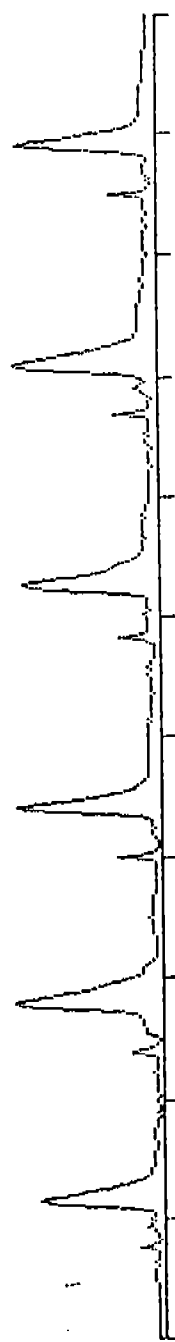
Plot of data file: E:AMB99.PTS

te: 09-07-1988 Time: 15:57:40

Sample Name: 70.15 mg/L as MeS

Start Time= 0.02 Stop Time= 9.75Min. Scale= 10684Max. Scale= 15861





[Interface 1] 0-11 Min Scale: 50 mV
S#12417 I Processed: 09-07-1988 14:52:01, segment 1, cycle 6
RAW DATA SAVED IN FILE E:AMB96.PTS

***** AREA PERCENT REPORT *****

* Sample Name: S#12417 INLET RUN #1 - IMPINGERS Operator Initials: RNS
* Date: 09-07-1988 14:52:07 Method: FIDSCAN DATA FILE: E:AMB96.PTS
* Interface: 1 Cycles: 6 Channel#: 0 Vial#: N.A.
* Starting Peak Width: 5 Threshold: 1

* Instrument Type: IKALUK MODEL 550 Column Type: 6' X 1/4" GLASS
* Solvent Description: EMPTY - (GLASS WOOL PLUGS)
* Operating Conditions: ISOTHERMAL OVEN 185-C, INJ. PORT 190-C, DET. 260-C
* Detector 0: FID Detector 1: NONE
* Misc. Information: He carr. 5.5scd, 2ul repl. inj.

Starting Delay: 0.00 Ending Retention Time: 11.00

Pk No.	Ret' Time	Peak	Area	B	Peak	Normalized	Area/ Height
		Area	%	L	Ht.	%	

Total Area: 0 Area Reject: %1000000000 One sample per 1.000 sec

START TIME= 10.983 START HEIGHT= 8636
 STOP TIME= 9.600 STOP HEIGHT= 8645
 AREA = 66280
 START TIME= 9.350 START HEIGHT= 8773
 STOP TIME= 7.767 STOP HEIGHT= 8661
 TA = 86040
 START TIME= 7.017 START HEIGHT= 8672
 STOP TIME= 5.967 STOP HEIGHT= 8841
 AREA = 71338
 START TIME= 5.383 START HEIGHT= 8646
 STOP TIME= 4.100 STOP HEIGHT= 8409
 AREA = 69393
 START TIME= 3.817 START HEIGHT= 8496
 STOP TIME= 3.267 STOP HEIGHT= 8540
 AREA = 4164
 START TIME= 3.250 START HEIGHT= 8581
 STOP TIME= 2.500 STOP HEIGHT= 8447
 AREA = 83206
 START TIME= 1.883 START HEIGHT= 8487
 STOP TIME= 0.817 STOP HEIGHT= 8448
 AREA = 62243

Plot of data file: E:AMB96.PTS

Date: 09-07-1988 Time: 14:55:01

Sample Name: S#12417 INLET R5

Start Time= 0.02 Stop Time= 11.00Min. Scale= 8309Max. Scale= 15429

E 19

AREA= 62243

E 18

AREA= 83206

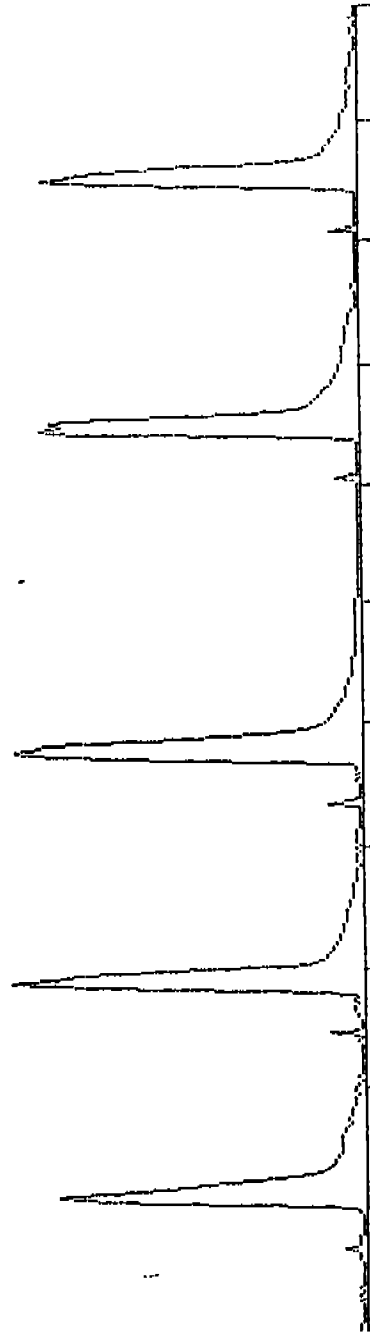
AREA= 4164

AREA= 69393

AREA= 71338

AREA= 86040

AREA= 66280



Interface 1] 0-11 Min Scale: 50 MV
S#12418 I Processed: 09-07-1988 15:08:09, segment 2, cycle 7
RAW DATA SAVED IN FILE E:AMB97.PTS

***** AREA PERCENT REPORT *****

* Sample Name: S#12418 INLET RUN #2 - IMPINGERS Operator Initials: RNS
* Date: 09-07-1988 15:08:16 Method:FIDSCAN DATA FILE: E:AMB97.PTS
* Interface: 1 Cycle#: 7 Channel#: 0 Vial#: N.A.
* Starting Peak Width: 5 Threshold: 1

* Instrument Type: INALUR MUDEL 550 Column Type: 6' X 1/4" GLASS
* Solvent Description: EMPTY - (GLASS WOOL PLUGS)
* Operating Conditions: ISOTHERMAL OVEN 185-C, INJ. PORT 190-C, DET. 260-C
* Detector 0: FID Detector 1: NONE
* Misc. Information: He carr. 5.5scoto, 2uL repl. inj.

Starting Delay: 0.00 Ending Retention Time: 11.00

117

Pk No.	Ret Time	Peak Area	Area %	B L	Peak Ht.	Normalized %	Area/Height
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Total Area: 0 Area Rejec %1000000000 One sample per 000 sec.

Areas, times, and heights stored in: E:AMB97.ATB
DATA FILE E:AMB97.HDR TAKEN 09-07-1988 15:08:16
NEW PEAK WIDTH = 10

118

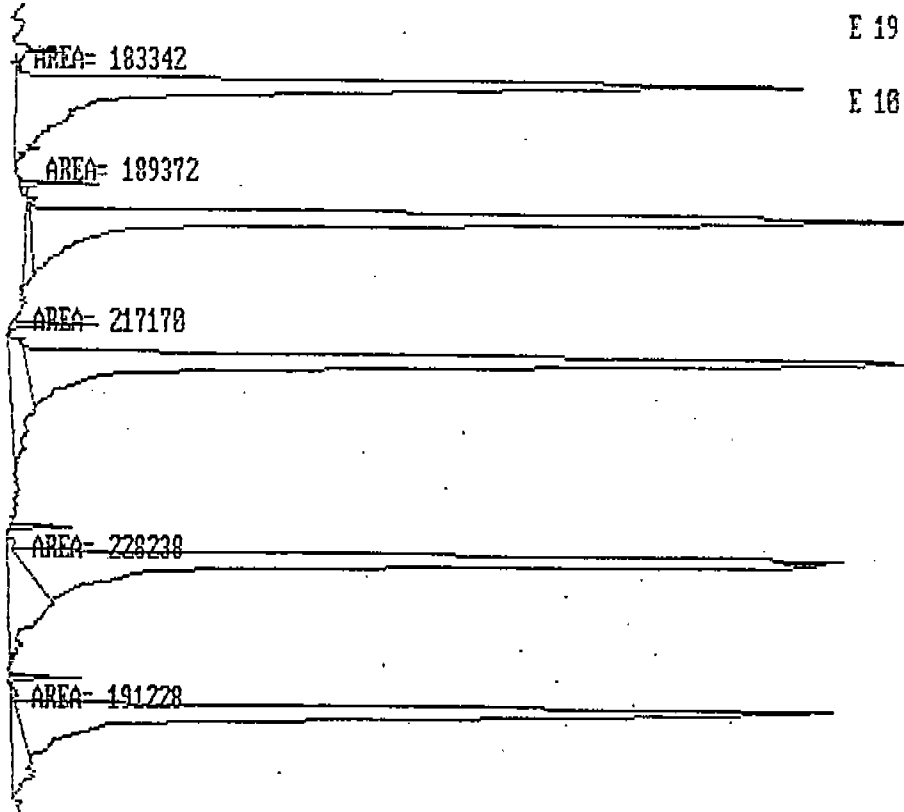
START TIME= 10.700 START HEIGHT= 8416
STOP TIME= 9.200 STOP HEIGHT= 8370
EA = 191228
START TIME= 8.917 START HEIGHT= 8346
STOP TIME= 7.150 STOP HEIGHT= 8281
AREA = 228238
START TIME= 6.300 START HEIGHT= 8431
STOP TIME= 4.467 STOP HEIGHT= 8279
AREA = 217170
START TIME= 3.900 START HEIGHT= 8579
STOP TIME= 2.500 STOP HEIGHT= 8633
AREA = 189372
START TIME= 2.217 START HEIGHT= 8406
STOP TIME= 0.817 STOP HEIGHT= 8442
AREA = 183342

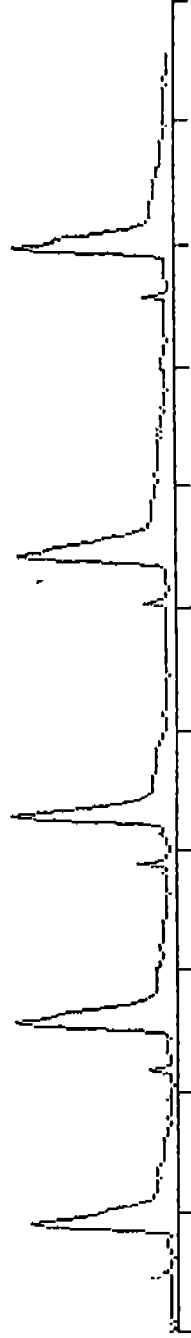
Plot of data file: E:AMB97.PTS

Date: 09-07-1988 Time: 15:10:22

Sample Name: S#12418 INLET R5

Start Time= 0.02 Stop Time= 11.00Min. Scale= 8162Max. Scale= 25419





[Interface 1] 0-11 Min Scale: 50 mV
S#12419 I Processed: 09-07-1988 15:24:22, segment 3, cycle 8
RAW DATA SAVED IN FILE E:AMB98.PTS

***** AREA PERCENT REPORT *****

* Sample Name: S#12419 INLET RUN #3 - IMPINGERS Operator Initials: RNS
* Date: 09-07-1988 15:24:29 Method: FIDSCAN DATA FILE: E:AMB98.PTS
* Interface: 1 Cycle#: 8 Channel#: 0 Vial#: N.A.
* Starting Peak Width: 5 Threshold: 1

* Instrument Type: TRACOR MODEL 550 Column Type: 6" X 1/4" GLASS
* Solvent Description: EMPTY - (GLASS WOOL PLUGS)
* Operating Conditions: ISOTHERMAL OVEN 185-C, INJ. PORT 190-C, DET. 260-C
* Detector 0: FID Detector 1: NONE
* Misc. Information: He carr. 5.5scoto, 2uL repl. inj.

Starting Delay: 0.00 Ending Retention Time: 11.00

Pk No.	Ret Time	Peak	Area	B	Peak	Normalized	Area/
		Area	%	L	Ht.	%	Height

Total Area: 0 Area Reject: %1000000000 One sample per 1.000 sec

Areas, times, and heights stored in: E:AMB98.ATB

GA FILE E:AMB97.HDR TAKEN 09-07-1988 15:08:16
DATA FILE E:AMB98.HDR TAKEN 09-07-1988 15:24:29
NEW PEAK WIDTH = 10

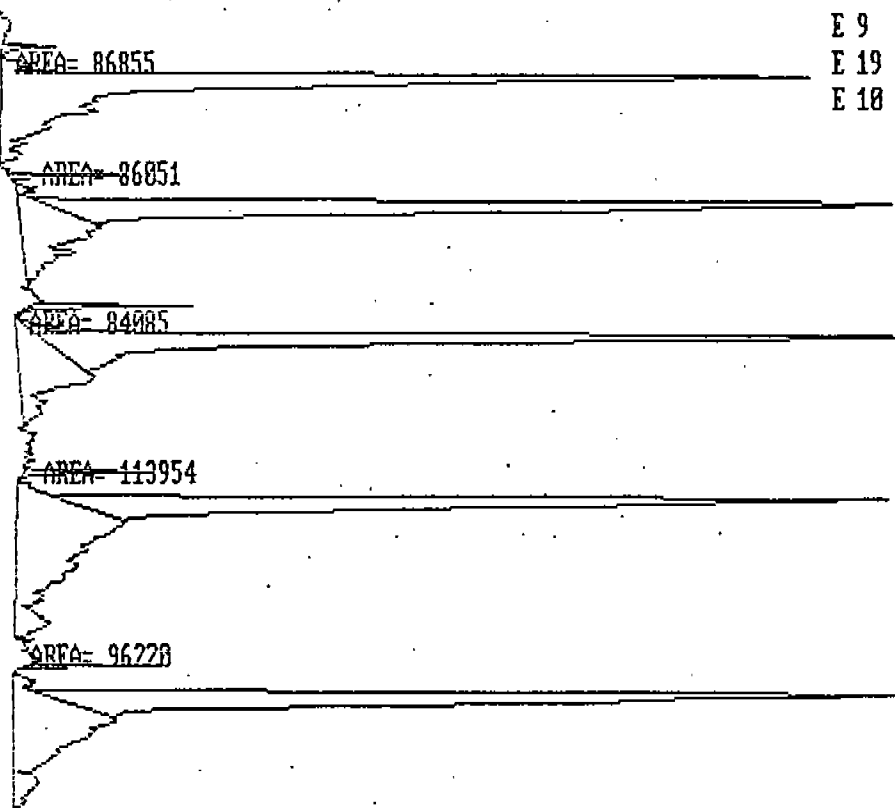
START TIME=	10.450	START HEIGHT=	8322
STOP TIME=	8.700	STOP HEIGHT=	8320
AREA =	96220		
START TIME=	8.217	START HEIGHT=	8334
STOP TIME=	6.150	STOP HEIGHT=	8350
AREA =	113954		
START TIME=	5.433	START HEIGHT=	8412
STOP TIME=	4.000	STOP HEIGHT=	8339
AREA =	84085		
START TIME=	3.633	START HEIGHT=	8446
STOP TIME=	2.283	STOP HEIGHT=	8352
AREA =	86051		
START TIME=	2.050	START HEIGHT=	8221
STOP TIME=	0.650	STOP HEIGHT=	8243
AREA =	86855		

Plot of data file: E:AMB98.PTS

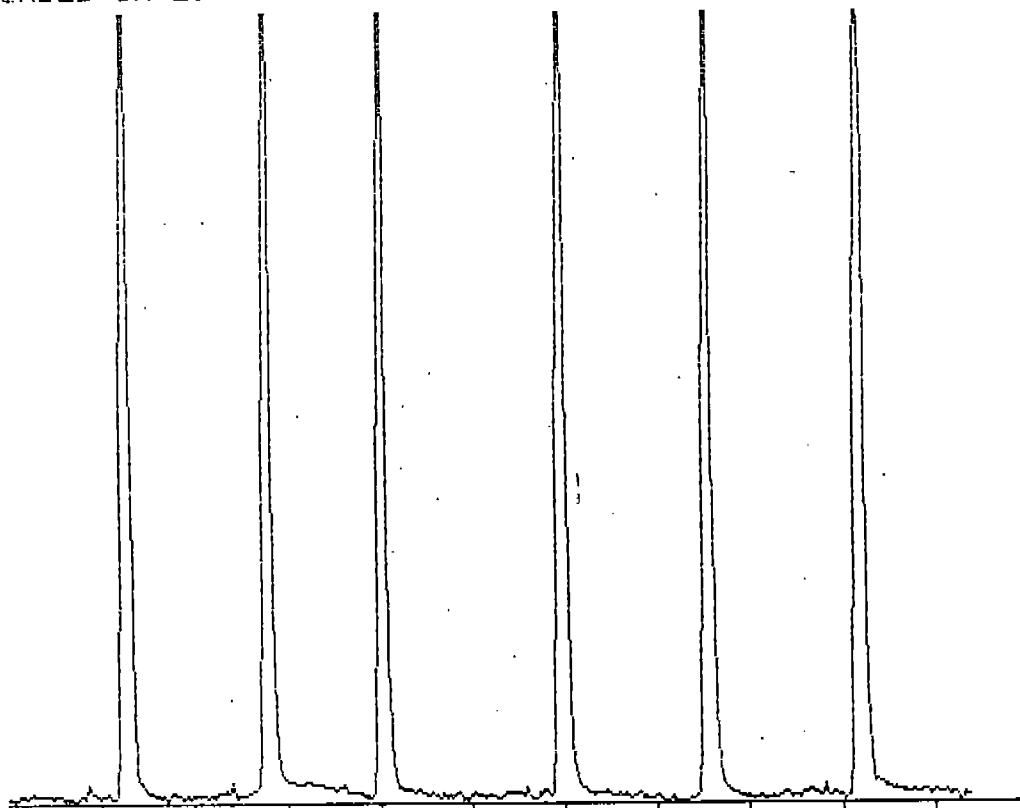
Date: 09-07-1988 Time: 15:28:22

Sample Name: S#12419 INLET R5

Start Time= 0.02 Stop Time= 10.53Min. Scale= 8091Max. Scale= 15752



SEQUENCE RECORDED IN E:AMB.SEO



[Interface 1] 0-11 Min Scale: 50 Mv

1169 mg/L Processed: 09-07-1988 16:15:56, segment 1, cycle 10

RAW DATA SAVED IN FILE E:AMB910.PTS

***** AREA PERCENT REPORT *****

 * Sample Name: 1169 mg/L as Methane Post - Cal. Operator Initials: RNS
 * Date: 09-07-1988 16:16:03 Method:FIDSCAN DATA FILE: E:AMB910.PTS
 * Interface: 1 Cycle#: 10 Channel#: 0 Vial#: N.A.
 * Starting Peak Width: 5 Threshold: 1

 * Instrument Type: TRACOR MODEL 550 Column Type: 6' X 1/4" GLASS
 * Solvent Description: EMPTY - (GLASS WOOL PLUGS)
 * Operating Conditions: ISOTHERMAL OVEN 185-C, INJ. PORT 190-C, DET. 260-
 * Detector 0: FID Detector 1: NONE
 * Misc. Information: He carr. 5.5scm, 2uL repl. inj.

 Starting Delay: 0.00 Ending Retention Time: 11.00

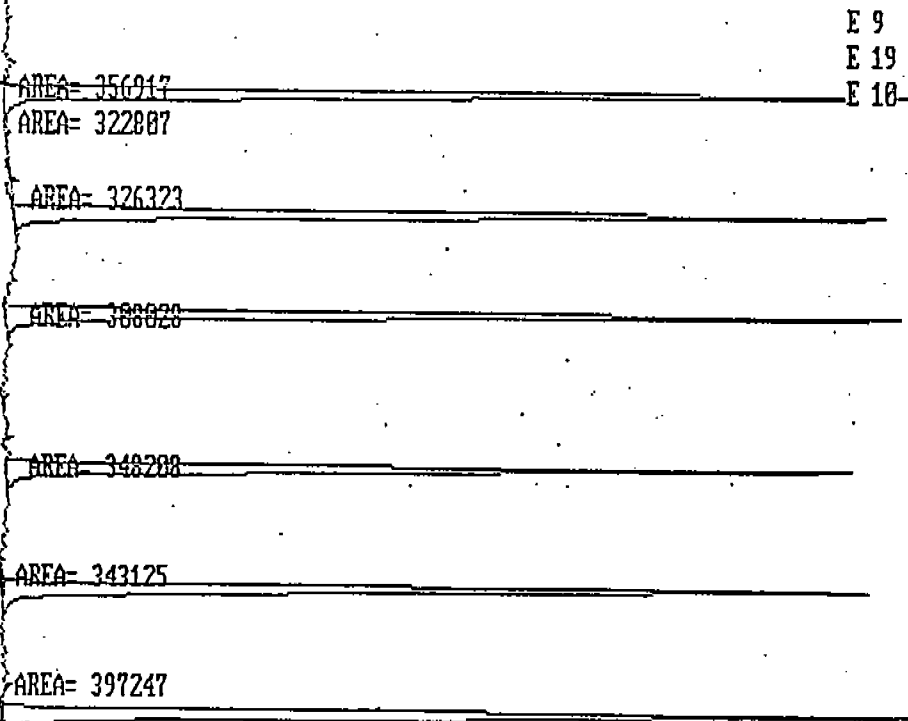
Pk No.	Ret Time	Peak Area	Area %	B L	Peak Ht.	Normalized %	Area/ Height
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Total Area:		0	Area Reject: %1000000000		One sample per	1.000
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Areas, times, and heights stored in: E:AMB910.ATB

FW PEAK WIDTH = 10
RT TIME= 9.850 START HEIGHT= 11240
STOP TIME= 9.017 STOP HEIGHT= 10751
REA = 397247
START TIME= 7.967 START HEIGHT= 10935
STOP TIME= 7.317 STOP HEIGHT= 10734
REA = 343125
START TIME= 6.433 START HEIGHT= 11264
STOP TIME= 5.850 STOP HEIGHT= 11081
REA = 348208
START TIME= 4.450 START HEIGHT= 11236
STOP TIME= 3.883 STOP HEIGHT= 10927
REA = 308028
START TIME= 3.100 START HEIGHT= 11740
STOP TIME= 2.617 STOP HEIGHT= 11182
REA = 326323
STOP TIME= 1.700 STOP HEIGHT= 10746
~~REA = 322887~~
START TIME= 1.700 START HEIGHT= 10746
STOP TIME= 1.133 STOP HEIGHT= 10831
REA = 356917

lot of data file: E:AMB910.FTS
ate: 09-07-1988 Time: 16:18:43
ample Name: 1169 mg/L as Met5
tart Time= 0.02 Stop Time= 10.32Min. Scale= 10442Max. Scale= 75398

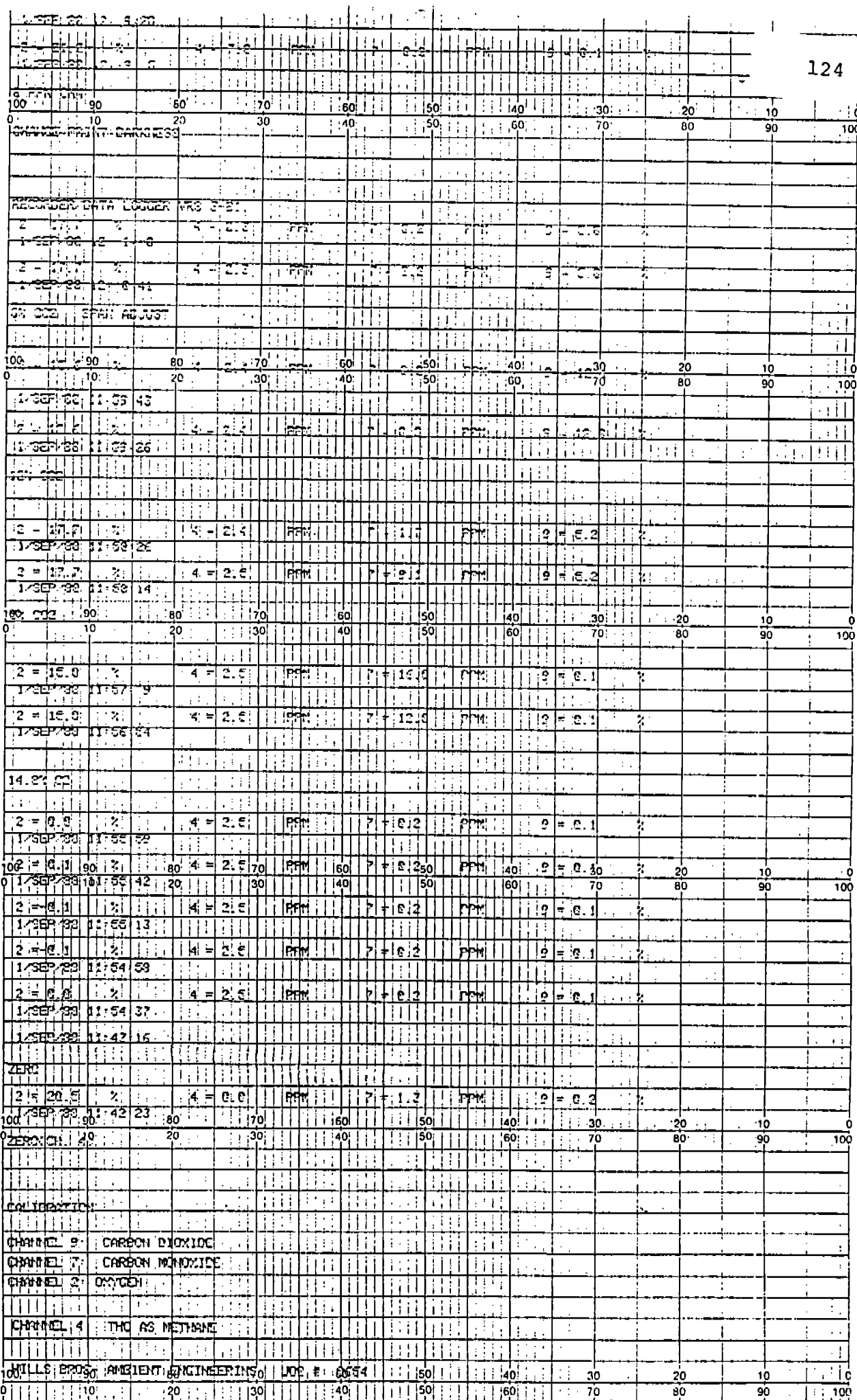


Sample: Hills Brothers Plant, 80L Tedlar Bags Sampled 8/31/88

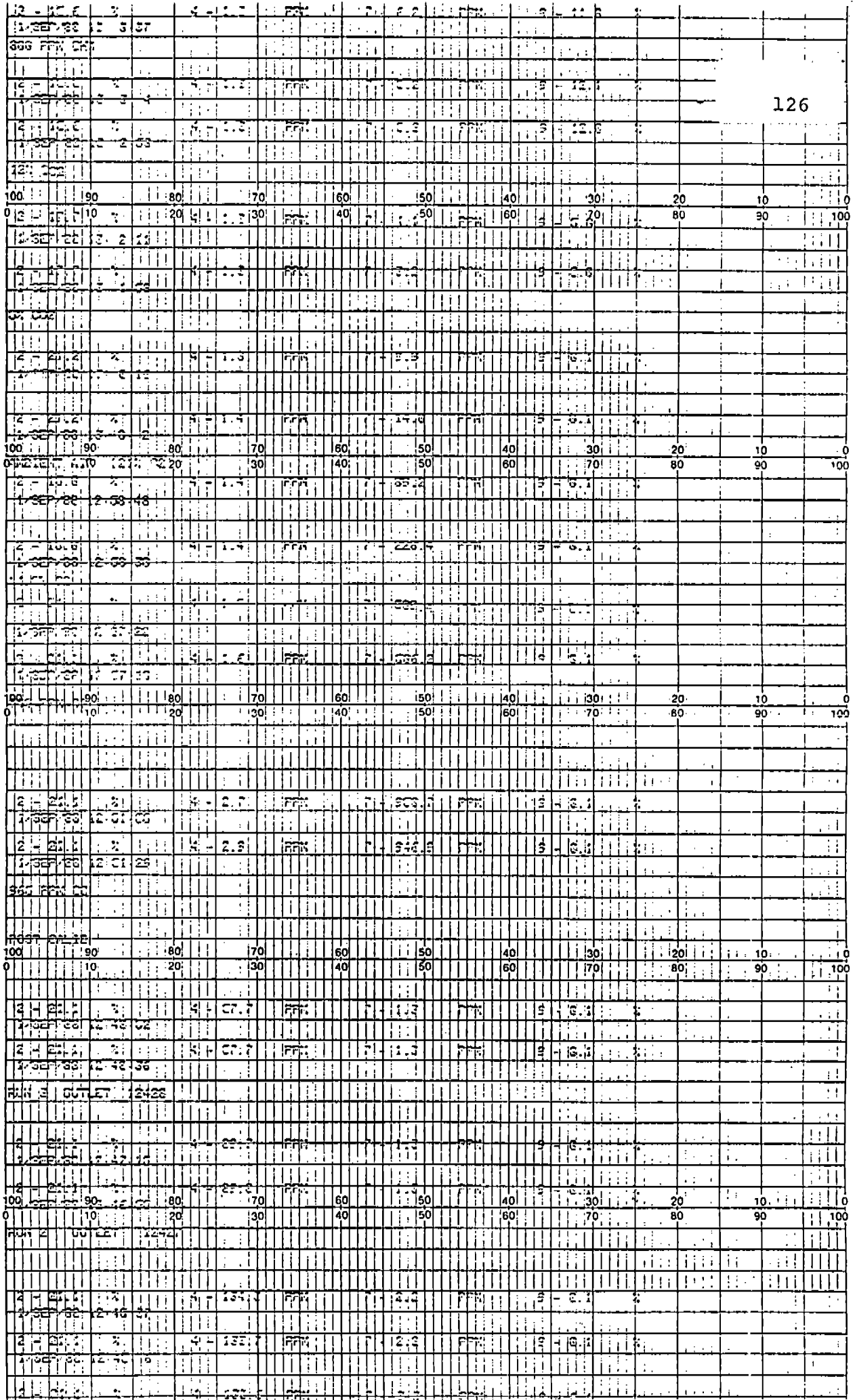
Method:

<u>RECON</u> <u>ID</u>	<u>Run</u> <u>No.</u>	<u>Sample</u> <u>Location</u>	<u>Total</u> <u>Hydrocarbons</u> <u>as methane</u>	<u>Carbon</u> <u>Monoxide</u> <u>ppm</u>	<u>Oxygen</u> <u>%</u>	<u>Carbon</u> <u>Dioxide</u> <u>%</u>
12423	1	Inlet	275	462	17.0	2.7
12424	2	Inlet	526	628	16.8	2.7
12425	3	Inlet	490	610	16.5	2.9
12426	1	Outlet	134	2.2	21.1	0.1
12427	2	Outlet	90	1.3	21.1	0.1
12428	3	Outlet	58	1.3	21.1	0.1
Detection Limit			1.	1.0	0.1	0.1

Samples from this project will be retained for sixty days from the date of this report unless otherwise directed.



TOLL FREE IN U.S.: (800) 245-5101 FAX (412) 361-7220



100	90	80	70	60	50	40	30	20	10	0
0	10	20	30	40	50	60	70	80	90	100
2nd LTR 5501										
2 - 2.2	1	4 - 6.2	FRM	7 - 10.2	FRM	8 - 12.1	2			
1-SEP-88	12 18 33									
2 - 2.2	2	4 - 6.2	FRM	7 - 10.2	FRM	8 - 12.1	2			
1-SEP-88	12 18 10									
2 - 2.2	3	4 - 6.2	FRM	7 - 10.2	FRM	8 - 12.1	2			
1-SEP-88	12 18 11									
1-SEP-88	12 18 35									
2nd LTR 5502										
2 - 2.2	1	4 - 6.2	FRM	7 - 10.2	FRM	8 - 12.1	2			
1-SEP-88	12 18 10									
2 - 2.2	2	4 - 6.2	FRM	7 - 10.2	FRM	8 - 12.1	2			
1-SEP-88	12 18 13									
2nd LTR 5503										
2 - 2.2	1	4 - 6.2	FRM	7 - 10.2	FRM	8 - 12.1	2			
1-SEP-88	12 18 10									
2 - 2.2	2	4 - 6.2	FRM	7 - 10.2	FRM	8 - 12.1	2			
1-SEP-88	12 18 10									
2nd LTR 5504										
2 - 2.2	1	4 - 6.2	FRM	7 - 10.2	FRM	8 - 12.1	2			
1-SEP-88	12 18 10									
2 - 2.2	2	4 - 6.2	FRM	7 - 10.2	FRM	8 - 12.1	2			
1-SEP-88	12 18 10									
2nd LTR 5505										
2 - 2.2	1	4 - 6.2	FRM	7 - 10.2	FRM	8 - 12.1	2			
1-SEP-88	12 18 10									
2 - 2.2	2	4 - 6.2	FRM	7 - 10.2	FRM	8 - 12.1	2			
1-SEP-88	12 18 10									
2nd LTR 5506										
2 - 2.2	1	4 - 6.2	FRM	7 - 10.2	FRM	8 - 12.1	2			
1-SEP-88	12 18 10									
2 - 2.2	2	4 - 6.2	FRM	7 - 10.2	FRM	8 - 12.1	2			
1-SEP-88	12 18 10									
2nd LTR 5507										
2 - 2.2	1	4 - 6.2	FRM	7 - 10.2	FRM	8 - 12.1	2			
1-SEP-88	12 18 10									
2 - 2.2	2	4 - 6.2	FRM	7 - 10.2	FRM	8 - 12.1	2			
1-SEP-88	12 18 10									
2nd LTR 5508										
2 - 2.2	1	4 - 6.2	FRM	7 - 10.2	FRM	8 - 12.1	2			
1-SEP-88	12 18 10									
2 - 2.2	2	4 - 6.2	FRM	7 - 10.2	FRM	8 - 12.1	2			
1-SEP-88	12 18 10									
2nd LTR 5509										
2 - 2.2	1	4 - 6.2	FRM	7 - 10.2	FRM	8 - 12.1	2			
1-SEP-88	12 18 10									
2 - 2.2	2	4 - 6.2	FRM	7 - 10.2	FRM	8 - 12.1	2			
1-SEP-88	12 18 10									
2nd LTR 5510										
2 - 2.2	1	4 - 6.2	FRM	7 - 10.2	FRM	8 - 12.1	2			
1-SEP-88	12 18 10									
2 - 2.2	2	4 - 6.2	FRM	7 - 10.2	FRM	8 - 12.1	2			
1-SEP-88	12 18 10									
2nd LTR 5511										
2 - 2.2	1	4 - 6.2	FRM	7 - 10.2	FRM	8 - 12.1	2			
1-SEP-88	12 18 10									
2 - 2.2	2	4 - 6.2	FRM</							

