

Note: This is a reference cited in AP 42, *Compilation of Air Pollutant Emission Factors, Volume I Stationary Point and Area Sources*. AP42 is located on the EPA web site at www.epa.gov/ttn/chief/ap42/

The file name refers to the reference number, the AP42 chapter and section. The file name "ref02_c01s02.pdf" would mean the reference is from AP42 chapter 1 section 2. The reference may be from a previous version of the section and no longer cited. The primary source should always be checked.

AP-42 Section 9.13.2
Reference 10
Report Sect. _____
Reference _____

**COMPLIANCE
STACK SAMPLING REPORT**

For

**General Foods Corporation
Maxwell House Division
1125 Hudson Street
Hoboken, New Jersey 07030**

Source Tested:

Afterburner Inlet and Outlet

**In Fulfillment of
Purchase Order No. 3362-88-MHD**

RECON Project No. 0641

Test Date: January 31 and February 1, 1989

Report Date: March 13, 1989

0641 (ST-K)

STACK SAMPLING REPORT FOR
General Foods Corporation
Maxwell House Division
Hoboken, New Jersey
on Afterburner Inlet and Outlet

INTRODUCTION

The above referenced locations were sampled for particulates. The outlet stack was also sampled for carbon monoxide and total hydrocarbon emissions on January 31 and February 1, 1989. This report contains the following information.

	PAGE
SUMMARY	2
PERSONNEL AND CERTIFICATIONS	3
SAMPLING LOCATIONS	4
VELOCITIES/FLOW RATES	6
CYCLONIC FLOW CHECK	8
GAS COMPOSITION	10
PARTICULATE EMISSIONS	12
HYDROCARBON AND CARBON MONOXIDE EMISSIONS	14
PROCESS INFORMATION	15
ALLOWABLE EMISSIONS	20
PROTOCOL/PROCEDURES	21
CALIBRATION DATA	34
ORIGINAL DATA AND CALCULATION SHEETS	48

SUMMARY

The following results were obtained:

<u>INLET</u>			
Run No.	1	2	3
Date	1/31/89	2/1/89	2/1/89
Time	1000-1145	0802-0921	1047-1247
<u>Emissions Data</u>			
<u>Particulates</u>			
pounds/hour	0.49	0.66	0.44
grains/dscf	0.035	0.046	0.032
grains/scf	0.032	0.042	0.030
<u>OUTLET</u>			
Run No.	1	2	3
Date	1/31/89	2/1/89	2/1/89
Time	1000-1151	0750-0920	1045-1245
<u>Emissions Data</u>			
<u>Particulates</u>			
pounds/hour	0.19	0.28	0.12
grains/dscf	0.011	0.016	0.007
grains/scf	0.010	0.015	0.007
<u>Total Hydrocarbons</u>			
<u>(as methane)</u>			
pounds/hour	0.10	0.18	0.15
ppmv (wet)	18	33	28
ppmv (dry)	20	36	31
<u>Carbon Monoxide</u>			
pounds/hour	1.14	3.70	1.40
ppmv (wet)	121	384	150
ppmv (dry)	131	416	166
<u>Carbon Monoxide Emissions</u>			
<u>Corrected to 21% Oxygen</u>			
ppmv (dry)	236	741	334
<u>Afterburner Efficiency</u>			
Particulates, %	61.2	57.6	72.7

Samples from this project will be retained for sixty days from the date of this report unless otherwise directed.

PERSONNEL AND CERTIFICATIONS

Field sampling on this project was performed by:

P. F. Marshall

S. J. Culmo

C. D. Ruff

T. F. Mattei

T. P. Brown

Laboratory work on this project was performed by:

R. N. Schaffer

A. W. McNeel

Calculations and report preparation were by:

P. F. Marshall

The testing was observed by:

Rob Tenbrevilla
Staffard Stewart
Michael Ciosek

NJDEP
 NJDEP
 NJDEP

This Report is submitted by:

Peter F. Marshall

Peter F. Marshall
Manager, Senior Environmental Specialist

Frank W. Swetits
Frank W. Swetits
Vice President

Frank W. Swetitz
Vice President

Professional Engineer Certification

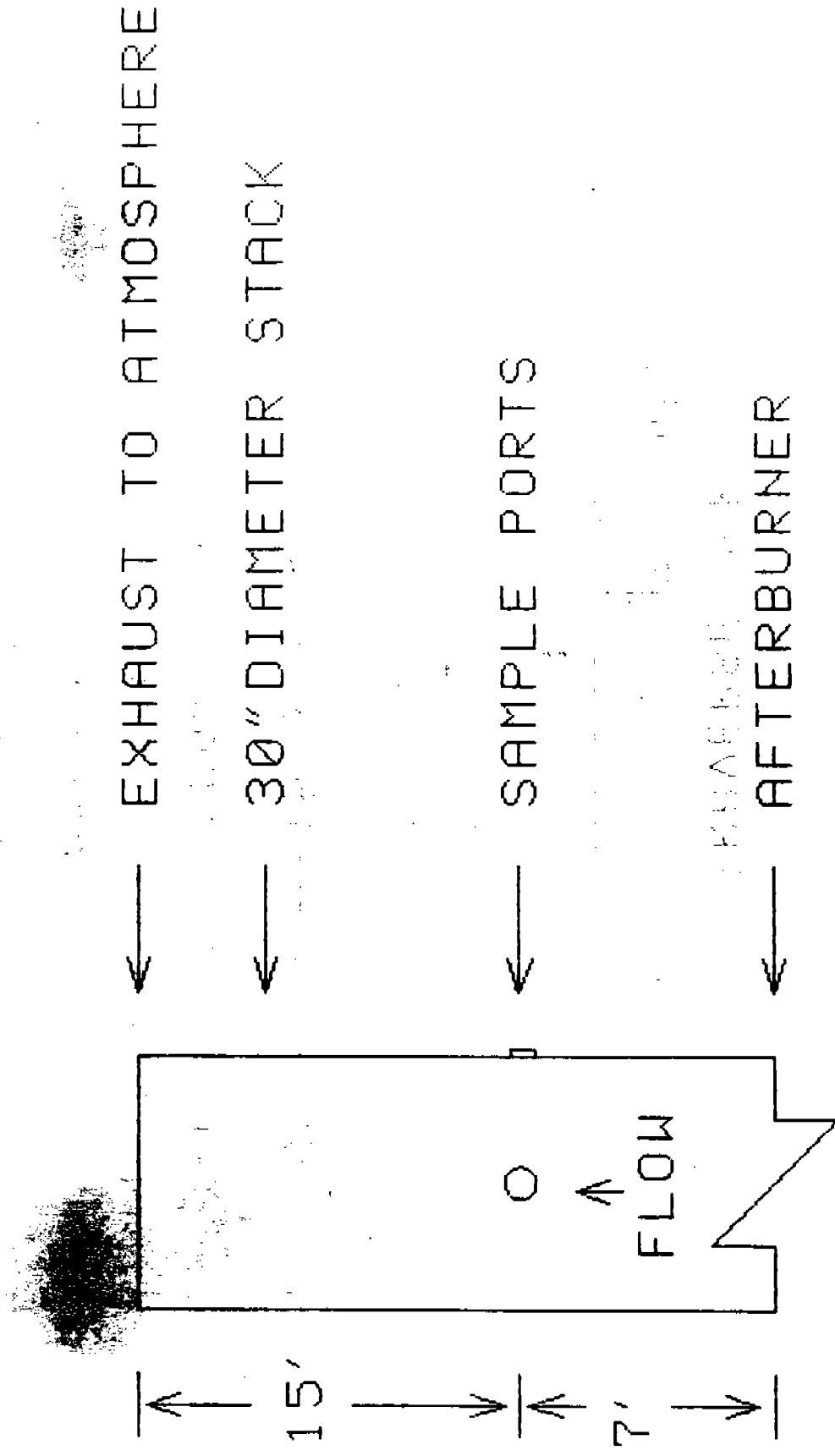
I am in responsible charge of RECON's stack test work, and have discussed and reviewed the procedures and results of this set of tests with the relevant field and laboratory personnel.

~~Norman J. Weinstein, P.E.~~
New Jersey License 19536

PFM/cp (ST-K)

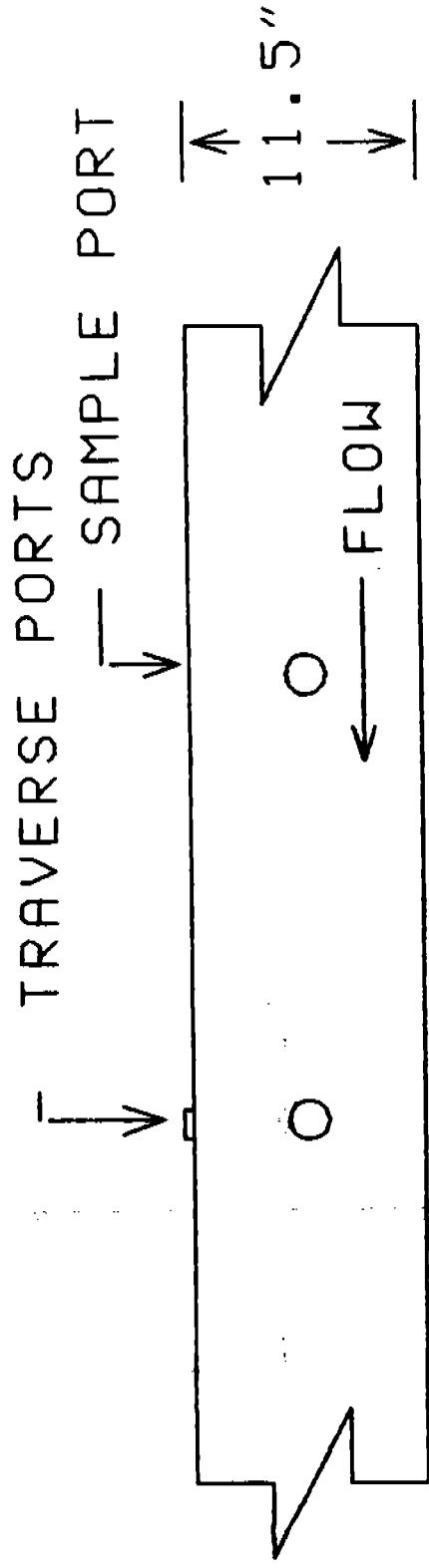
28

GENERAL FOODS CORPORATION
MAXWELL HOUSE DIVISION
AFTERBURNER OUTLET



EPA DISTANCE "A": 6.00
EPA DISTANCE "B": 2.80
SAMPLE POINTS: 24

GENERAL FOODS CORP.
MAXWELL HOUSE DIVISION
INCINERATOR OUTLET



6" 15.5" 52"

UPSTREAM DISTURBANCE: AFTERBURNER

DOWNSTREAM DISTURBANCE: CYCLONE

EPA DISTANCE "A": 0.52

EPA DISTANCE "B": 4.52

STACK DIAMETER: 11.5"

TRAVERSE POINTS: 24

SAMPLE POINTS: 1

VELOCITY AND FLOW RATE DATA - Inlet

Sample No.	1	2	3
Date	1/31/89	2/1/89	2/1/89
Time	1000-1145	0802-0921	1047-1247
Stack Diameter (in)	11.5	-----	-----
Stack Cross Section (sq ft)	0.72	-----	-----
Barometric Pressure ("Hg)	29.91	29.78	29.80
Average Stack Temperature (°F)	163	194	201
Stack Pressure ("H ₂ O-gage)	-4.40	-4.30	-4.20
Moisture (% vol)	9.8	9.0	9.0
Average Velocity (ft/sec)	49.4	53.2	52.4
Actual Flow Rate (acfm)	2,140	2,300	2,270
Standard Flow Rate (scfm)	1,800	1,840	1,790
Dry Standard Flow Rate (dscfm)	1,620	1,670	1,630

Standard Conditions are 70°F, 29.92 "Hg.

VELOCITY AND FLOW RATE DATA - Outlet

Sample No.	1	2	3
Date	1/31/89	2/1/89	2/1/89
Time	1000-1151	0750-0920	1045-1245
Stack Diameter (in)	30.0	-----	-----
Stack Cross Section (sq ft)	4.91	-----	-----
Barometric Pressure ("Hg)	29.91	29.78	29.80
Average Stack Temperature (°F)	1506	1513	1526
Stack Pressure ("H ₂ O-gage)	-0.02	-0.02	-0.02
Moisture (% vol)	7.9	7.6	9.3
Average Velocity (ft/sec)	27.5	28.0	27.2
Actual Flow Rate (acfm)	8,110	8,240	8,020
Standard Flow Rate (scfm)	2,180	2,200	2,130
Dry Standard Flow Rate (dscfm)	2,010	2,030	1,930

Standard Conditions are 70°F, 29.92 "Hg.

CYCLONIC FLOW - Inlet

<u>Angle, Degrees</u>		
<u>Point</u>	<u>Port A</u>	<u>Port B*</u>
1	0	-
2	2	-
3	4	-
4	4	-
5	2	-
6	2	-
7	4	-
8	4	-
9	5	-
10	7	-
11	5	-
12	2	-

Avg. 3.4

NOTE: Since the average value of the cyclonic flow check is less than 20 degrees, the location is an appropriate location to determine flow rate (U.S. EPA Method 1).

*Cyclonic flow could not be determined from this port because of the horizontal stack.

CYCLONIC FLOW - Outlet

Angle, Degrees

<u>Point</u>	<u>Port A</u>	<u>Port B</u>
1	5	8
2	3	7
3	2	7
4	2	4
5	2	4
6	3	3
7	3	4
8	7	6
9	7	5
10	6	6
11	4	7
12	<u>6</u>	<u>7</u>
	Avg. 4.2	6.2

NOTE: Since the average value of the cyclonic flow check is less than 20 degrees, the location is an appropriate location to determine flow rate (U.S. EPA Method 1).

CYCLONIC FLOW - Outlet

Angle, Degrees

<u>Point</u>	<u>Port A</u>	<u>Port B</u>
1	5	8
2	3	7
3	2	7
4	2	4
5	2	4
6	3	3
7	3	4
8	7	6
9	7	5
10	6	6
11	4	7
12	<u>6</u>	<u>7</u>
	Avg. 4.2	6.2

NOTE: Since the average value of the cyclonic flow check is less than 20 degrees, the location is an appropriate location to determine flow rate (U.S. EPA Method 1).

STACK GAS COMPOSITION - Inlet

Sample No.	1	2	3
Date	1/31/89	2/1/89	2/1/89
Time	1000-1151	0750-0920	1045-1245

% By Volume
(Dry Basis)

ONSITE FYRITE

CO ₂	0.5	0.0	0.0
O ₂	20.5	20.0	20.5
N ₂ (By Difference)	79.0	80.0	79.5

LAB ORSAT

CO ₂	0.0	0.0	0.0
O ₂	21.0	21.0	21.0
N ₂ (By Difference)	79.0	79.0	79.0

STACK GAS COMPOSITION - Outlet

Sample No.	1	2	3
Date	1/31/89	2/1/89	2/1/89
Time	1000-1145	0802-0921	1047-1247

ONSITE FYRITE

% By Volume
(Dry Basis)

CO ₂	4.0	6.0	5.0
O ₂	14.0	15.0	15.0
N ₂ (By Difference)	82.0	79.0	80.0

LAB ORSAT

CO ₂	5.4	5.8	6.0
O ₂	13.2	13.1	14.0
N ₂ (By Difference)	81.4	81.1	80.0

PARTICULATE EMISSIONS - Inlet

Sample No.	1	2	3
Date	1/31/89	2/1/89	2/1/89
Time	1000-1145	0802-0921	1047-1247

Sampling Data

Nominal Nozzle Size (in)	1/2 -----		
No. of Sampling Points	1 -----		
Sampling Time (min)	60 -----		
Sample Volume (dscf)	43.7 ^{41.56}	47.6 ^{44.5}	44.3 ^{41.9}
% Isokinetic	89	94	91

Emissions Data

<u>Particulates</u>			
Grains/dscf	0.0355	0.0463	0.0318
Grains/scf	0.0319	0.0421	0.0300
Pounds/hour	0.49	0.66	0.44

PARTICULATE EMISSIONS - Outlet

Sample No.	1	2	3
Date	1/31/89	2/1/89	2/1/89
Time	1000-1151	0750-0920	1045-1245

Sampling Data

Nominal Nozzle Size (in)	1/2	-----	
No. of Sampling Points	24	-----	
Sampling Time (min)	72	60	60
Sample Volume (dscf)	38.4	33.7	32.1
% Isokinetic	95	99	100

Emissions Data

Particulates

Grains/dscf	0.0113	0.0161	0.0073
Grains/scf	0.0104	0.0148	0.0066
Pounds/hour	0.19	0.28	0.12

HYDROCARBON AND CARBON MONOXIDE EMISSIONS - Outlet

Sample No.	1	2	3
Date	1/31/89	2/1/89	2/1/89
Time	1000-1151	0750-0920	1045-1245

Sampling Data

No. of Sampling Points	1	-----
Sampling Time (min)	60	-----
Sample Volume (dscf)	2.12	-----

Emissions Data

Total Hydrocarbons
(as methane)

pounds/hour	0.10	0.18	0.15
ppmv (wet)	18.5	36	31
ppmv (dry)	20.1	33	28

Carbon Monoxide

pounds/hour	1.14	3.70	1.40
ppmv (wet)	131	416	166
ppmv (dry)	121	384	150

PROCESS INFORMATION

The following process information was supplied to RECON by General Foods/Maxwell House Division personnel.

EMISSION TEST PRODUCTION REPORT FORM

I. Company Name MAXWELL HOUSE APC Plant ID# _____
Plant Location HOBOKEN _____
Certificate Number _____
Designation of Equipment PILOT PLANT AFTERBURNER

II. Emission Test Date(s) 31 JAN 89

Tests Conducted By:

Name of Firm RECON SYSTEMS

Business Address RT 202 N, PO BOX 460, Three Bridges, NJ 08887
Phone Number (201) 782-5960

Phone Number (201) 782-5960

Test Team Representatives Peter Marshall

Dave Ruff

Tom Brien

Tom Natto

Fuel Usage was about 2000 ft³/hr

Length of Test 6 hrs

	<u>Run #1</u>	<u>Run #2</u>	<u>Run #3</u>
Test Time (Start/Finish)	/	/	/

III. Certificate Operating Conditions

A. List Conditions

Achieved (Yes or No)

350 lb/hr
~~250~~ lbs/hr coffee
1500 °F

yes

B. Log of Certificate Conditions During Stack Test
(Record at least every 15 minutes)

Condition	Run #	Readout	Time of Recording
-----------	-------	---------	-------------------

[illegible]

IV. Equipment Operation/Process Parameters

Number of Sources Connected 2
Number of Sources Operating 2

Production Rate: Normal 200 + 150 = 350 lbs/hr
Maximum 350 lbs/hr

A. Raw Materials: Green whole beans

	Test Run #1	Test Run #2	Test Run #3
Usage Rate (lbs/hr)	<u>350 lbs/hr</u>	<u>350 lbs/hr</u>	<u>350 lbs/hr</u>
Breakdown (% by weight)	<u>200 lbs/hr</u>	<u>200 lbs/hr</u>	<u>200 lbs/hr</u>

B. Surface Coating:

Material Being Coated N/A
Type of Coating _____
Coating Rate (Gals/Hr) _____
Is Coating Altered (Yes or No) _____
With _____

Distance From Coating Head to Exhaust Duct N/A

C. Fuel Burning - Incineration:

Type of Fuel Natural Gas
Fuel Burning Rate _____ (lbs/hr), (gals/hr), (ft³/hr)
Fuel Additives None, % _____

Meter Reading
(if available)

Time

B. Additional Observations

Fugitive Emissions (Yes/No) _____

Equipment Location _____

Visible Emissions From Stack (Yes/No) _____

Odors Noticeable _____

Vicinity of Equipment (Yes/No) _____

Near Exhaust Stack (Yes/No) _____

Off Property (Yes/No) _____

VI. Samples

Type of Sample _____

Time of Sampling _____

Sampled By _____

Sample Taken From _____

To Be Analyzed For _____

Analyzed By _____

Form Information Supplied by: Name/Title (Please Print)

BRUNO G. PADOVANI, PROJECT ENGINEER

Signature(s)/Date

Bruno G. Padovani

DEP Usage Only

Rec'd By

Sample Rec'd
Date/Time

Rev'd By

ALLOWABLE EMISSIONS

The following allowable emissions are based on our understanding of the applicable regulatory rules and regulations. Since we are not always privy to the situation, these should not be accepted without confirmation from relevant sources.

<u>Particulate</u>	<u>Reference</u>	<u>Allowable</u>
Federal Regulations	_____	_____
State Regulations	_____	_____
State Permit	<u>X</u>	<u>0.15 pounds/hr</u> <u>99% Unit Efficiency</u>
<u>Sulfur Dioxide</u>		
Federal Regulations	_____	_____
State Regulations	_____	_____
State Permit	_____	_____
<u>Sulfur Trioxide and Sulfuric Acid</u>		
Federal Regulations	_____	_____
State Regulations	_____	_____
State Permit	_____	_____
<u>Nitrogen Oxides</u>		
Federal Regulations	_____	_____
State Regulations	_____	_____
State Permit	_____	_____
<u>Hydrocarbon (VOS, VOC)</u>		
Federal Regulations	_____	_____
State Regulations	_____	_____
State Permit	_____	_____
<u>Other:</u> _____		
Federal Regulations	_____	_____
State Regulations	_____	_____
State Permit	_____	_____

_____ We do not have sufficient information to determine allowable emissions.

PROTOCOL/PROCEDURES

Following is a copy of the original approved protocol.



0 0.25

State of New Jersey
DEPARTMENT OF ENVIRONMENTAL PROTECTION
DIVISION OF ENVIRONMENTAL QUALITY
CN 027, TRENTON, N.J. 08625

JORGE H. BERKOWITZ, Ph.D.
DIRECTOR

(609) 292-5383

July 14, 1988

Dear Mr. Savat

Enclosed is a copy of DEP's response to RECON's stack sampling protocol for your project #0041. Please submit to me a revision to your protocol reflecting all DEP required changes. Your cooperation in this matter is greatly appreciated. Please provide a copy of this letter to Peter Marshall.

Mr. Bruno S. Padovani
Project Engineer
General Foods Manufacturing Corporation
Maxwell House Division
1125 Hudson Street
Hoboken, New Jersey 07030

RE: Afterburner Stack
APC ID No. 10082
NJ Stack No. 068

Sincerely yours,
Bruno S. Padovani

Dear Mr. Padovani:

We have received the sampling and analytical protocol your company has submitted for the above referenced source. Emission tests are required to be conducted as a condition of approval of Permit No. P-82002.

Our review of the proposed procedures indicates several items which must be amended into the protocol prior to our approval. These items are as follows:

- 1) Emission tests for total hydrocarbons, as methane, must be conducted on the incinerator outlet. Sampling and analytical procedures to determine the total hydrocarbon emissions, must be submitted to our office for review and approval.
- 2) Carbon monoxide emission tests must follow the procedures outlined in EPA Reference Method 10.
- 3) Determination of oxygen concentrations must follow those outlined in EPA Reference Method Three.
- 4) Data on the determination of the absence of cyclonic flow must be presented to the on-site observer from this office prior to conducting the compliance tests.

You are required to respond to each item, in writing to our office. Until we have received and reviewed your comments, we can accept the submitted protocol.

If you have any questions please feel free to call me at (609) 530-4041.

Sincerely



Edward M. Choromanski
Chief

Bureau Technical Services

c Byron Sullivan (M.R.O.)

RECON SYSTEMS, INC.

0 0.3

Route 202 North, P.O. Box 460
Three Bridges, N.J. 08887
201-782-5900

New England 617-752-4217 Pennsylvania 215-433-5511

August 1, 1988

Mr. Edward M. Choromanski
NEW JERSEY DEPARTMENT OF
ENVIRONMENTAL PROTECTION
Technical Services Section
380 Scotch Road
W. Trenton, NJ 08628

Re: General Foods Corporation
Afterburner Stack
APC ID No. 10082
NJ Stack No. 068

RECON Project No. 0641

Dear Mr. Choromanski:

We have received your letter dated July 14, 1988 regarding protocol amendments for compliance testing at the above mentioned facility.

Response to these items are as follows:

1. The afterburner outlet will be tested in triplicate for total hydrocarbons as methane.
Proposed number of sampling points 1
Proposed time per sampling point 60
Proposed total stack gas sample size 2.12 dry standard ft³

Please see diagram of sampling train

Condensable material recovered in the impinger catches will be determined by a gas chromatograph equipped with a flame ionization detector for determination of total hydrocarbons.

Gas bag samples will be directly injected into the GC/FID via a calibrated sample loop. Total hydrocarbon concentrations will be determined as above. Concentrations of both phases will be totaled and used to calculate emissions. Copies of chromatograms will be included in our final report showing identified responses plus any other unidentified peaks.

ENGINEERING, CONSULTING, LABORATORY,
PILOT PLANT, PLANT TEST SERVICES

POLLUTION CONTROL, WASTE DISPOSAL
RESOURCE RECOVERY, CHEMICAL PROCESS SYSTEMS

Mr. Edward M. Choromanski

-2-

August 1, 1988

2. We agree.

3. We agree.

4. We agree.

We anticipate a test date during the week of August 22, 1988, Please advise us of a test date that is convenient with your office.

Feel free to call if you have any questions or comments.

Very truly yours,

Richard F. Toro

Richard F. Toro
Executive Vice President

Peter F. Marshall
Per Peter F. Marshall
Senior Environmental Specialist

PFM/cp

cc: Bruno Padovani
General Foods Corporation
Maxwell House Division
1125 Hudson Street
Hoboken, NJ 07030



0022

State of New Jersey
DEPARTMENT OF ENVIRONMENTAL PROTECTION
DIVISION OF ENVIRONMENTAL QUALITY
CN 027, TRENTON, N.J. 08625

JORGE H. BERKOWITZ, Ph.D.
DIRECTOR

August 9, 1988

(609) 292-6383

Mr. Richard F. Toro
Executive Vice President
Recon Systems, Inc.
P.O. Box 460
Three Bridges, New Jersey 08887

RE: General Foods Corporation
APC Plant ID No. 10082
NJ Stack No. 067 and 068

Dear Mr. Toro:

We have received your letter dated August 1, 1988 regarding the amendment to the emission test protocol for the above referenced facility. Our review of this additional information incorporating the previous submittal dated July 11, 1988 indicates the sampling and analytical procedures are acceptable.

In addition to the sampling and analytical protocol your company or a representative of General Foods, is required to complete the emission test production form which I have enclosed. The completed form must be sent to the Regional Office where the facility is located. A copy of the form must be included into the final test report.

You are required to contact this office to arrange a mutually acceptable test date, so that representatives of the Department may witness the tests.

If you have any questions, please feel free to call me at (609) -530-4041.

Sincerely,

Edward M. Choromanski
Chief
Bureau of Technical Services

c Byron Sullivan

RECON SYSTEMS, INC.

0 027

Route 202 North, P.O. Box 460
Three Bridges, N.J. 08887
201-782-5900

New England 617-752-4217 Pennsylvania 215-433-5511

STACK TEST PROTOCOL SUBMITTAL

NEW JERSEY DEPARTMENT OF
ENVIRONMENTAL PROTECTION
Technical Services Section
380 Scotch Road
W. Trenton, NJ 08628

Attn: Edward Choromanski

RE: General Foods/ Maxwell
House Division
1125 Hudson Street
Hoboken, NJ 07030

Contact: John LaSalle
Phone No. 201-420-3731

RECON Project No. 0641

This protocol is submitted for stack testing planned by RECON SYSTEMS, INC. for the above referenced client.

Source to be tested: Afterburner Inlet and Outlet
ID No.: 068

Certificate Numbers: 082002

Approximate Date of Testing: August 1988

For Isokinetic Testing:

Inlet

Stack diameter: 12"
Nearest upstream disturbances: 6"
Nearest downstream disturbances: 5'
EPA Distance "A": 0.5 - EPA Distance "B": 5.0
Proposed number of sampling points: 24
Proposed time per sampling point: 3 minutes
Proposed total stack gas sample size: -35.00 dry standard ft³

Outlet

Stack diameter: 36"
Nearest upstream disturbances: 15'
Nearest downstream disturbances: 7'
EPA Distance "A": 5.00 - EPA Distance "B": 2.33
Proposed number of sampling points: 24
Proposed time per sampling point: 3 minutes
Proposed total stack gas sample size: -35.00 dry standard ft³

ENGINEERING, CONSULTING, LABORATORY,
PILOT PLANT, PLANT TEST SERVICES

POLLUTION CONTROL, WASTE DISPOSAL
RESOURCE RECOVERY, CHEMICAL PROCESS SYSTEMS

Sampling Program

Three (3) one-hour compliance tests will be conducted for particulates using New Jersey Air Test method 1. Temperatures of the stack, probe, filter inlet, filter box and filter outlet will be recorded. Flow rates, O₂, CO₂, N₂ (by difference) will also be recorded. Impinger Numbers 1 and 2 will have 100 mls each H₂O. Impinger Number 3 empty, Impinger Number 4 will contain 200 gms of silica gel. Non-cyclonic flow will be field verified. Calibration data will be made available to the onsite observer.

Carbon monoxide and oxygen concentrations will be determined by extracting a gas sample from the stack at one liter per minute for sixty minutes in triplicate. Samples will be analyzed within a 48-hour period.

Source Operation Record Keeping

Responsibility of A Owner RECON

☐ Production rate
☐ Fuel usage
☒ Incineration feed rate
☐ Steam production
☒ Operating parameters (temperatures, pressures, flows, etc.)
☐ Other

The following are attached if available:

1. Test procedures proposed
2. Stack diagram
3. Permits or applications
4. Process description

This protocol submitted by:

Frank W. Gattita
 Frank W. Gattita
 Manager, Field Testing

Peter F. Marshall
 Peter F. Marshall
 Senior Environmental Specialist

FWS/PFM:cac
 (PRO-3)

STACK TESTING PROCEDURES CHECKLIST

0 0.29

Particulate

Emissions: ☐ US EPA 5
☐ US EPA 17
☒ N.J. Method 1
☐ N.J. Method 5 (draft)
☐ Plus impinger catch
☐ Plus aqueous and organic impinger catch
☐ Other _____
 Probe Material Glass

Velocity: ☐ Standard pitot tube and manometer
☒ "S" pitot tube and manometer
☐ Other: _____
☒ Cyclonic Flow Check ☒ Yes ☐ No

Temperature: ☒ Thermocouple
☐ Temperature gage
☐ Process indicator

Gas

Composition: ☒ Onsite fyrite
☒ Grab sample and lab orsat
☐ Integrated sample and lab orsat
☐ Integrated and traversed sample and lab orsat
☐ Oxygen by Infrared Industries 2200 Electrochemical Analyzer

Particle

Sizing: ☐ Instack cascade impactor
☐ Heated out of stack cascade impactor
☐ Plus impinger catch
☐ Plus aqueous and organic impinger catch

Sulfur Oxide

Emissions: ☐ US EPA 6
☐ US EPA 8
☐ Sulfite Corrections Made
☐ Controlled condensation for SO₂
☐ US EPA 6 ☐ or 8 ☐ combined with
☐ US EPA 5 ☐ or 17 ☐ or particle sizing ☐

Nitrogen Oxide

Emissions: ☐ US EPA 7 ☐ A, ☐ B, ☐ C, ☐ D, ☐ E
☐ Chemiluminescent monitor
☐ US EPA 20 (Chemiluminescent Monitor)

Hydrogen Chloride (HCl)

Emissions: ☐ API 767-54
☐ Cl⁻ analysis of particulate test wet catch
☐ Other _____

Hydrocarbon

Emissions: ☐ N.J. Method 3
☐ RECON Method 2
☐ Integrated gas bag direct and lab GC
☐ Grab sample gas bag direct and lab GC
☐ Onsite GC direct ☐ detector
☐ Onsite Continuous Monitor (FID)

Metal Emissions ☐ AA determination on filter and probe wash
☐ AA determination on impinger catch

Carbon Monoxide

Emissions: ☒ Thermal Conductivity analysis of "Gas Composition" sample(s)
☐ Onsite Continuous Monitor

Opacity:

☐ N.J. Method 2
☐ U.S. EPA Method 9

Calibrations: Dry gas meters and orifice, pitot tubes, thermocouples and nozzle calibrations will be supplied with the test report unless test is unofficial.

Comments:



0 030

State of New Jersey
DEPARTMENT OF ENVIRONMENTAL PROTECTION
DIVISION OF ENVIRONMENTAL QUALITY
CN 027, TRENTON, N.J. 08625

JORGE H. BERKOWITZ, Ph.D.
DIRECTOR

February 23, 1988

(609) 292-3383

Mr. Walter Johnston
Maxwell House Div.,
General Foods Corp.
1125 Hudson Street
Hoboken, NJ 07030

Dear Mr. Johnston:

This letter is to advise you that a Permit to Construct, Install or Alter Control Apparatus or Equipment and Certificate to Operate Control Apparatus or Equipment has been approved by the Bureau of New Source Review as follows:

Company Name: General Foods Corp.

Plant Location: Maxwell House Div., Hoboken, NJ

Company Designation of Stack: Afterburner Stack 068

Approval Date: 1-28-86

Log Number: 86-2163 ID 10082

Certificate Status: 90 Day Conditional - see attached

You will be sent form VEM-017 at a later date. Form VEM-017 will include your New Jersey Plant ID Number, New Jersey Stack Number, and Permit/Certificate Number.

If you have any questions regarding this approval, please contact this bureau at (609-292-6716) and refer to the Log Number above.

Sincerely,

Richard Craig
Richard Craig, Chief
Bureau of New Source Review

RC:lsk
cc: P. Zigrand
MRO
File

Afterburner Conditions 100 No. 186-1158

The permit and certificate will be conditioned with the following stipulations:

1. The afterburner shall have a minimum design destruction efficiency of 99 percent for particulate emissions. The particulate emissions may not exceed 0.15 lb/hr.

2. The afterburner shall be designed to operate at a minimum temperature of 1700 degrees F with a minimum residence of 0.5 seconds.

3. A continuous temperature monitor and recorder shall be installed and operated in the afterburner. The thermometer shall be installed in the exit from the combustion chamber.

4. Continuous carbon monoxide and oxygen monitors and recorders shall be installed and operated in the afterburner stack. The Department reserves its right and authority to request the installation of a continuous total hydrocarbon monitor and recorder if necessary. The company may propose to the Department for approval a surrogate method for determining oxygen levels in the afterburner exhaust gases for the purposes of establishing steady state combustion conditions. Such methods may include periodic testing by Orsat analysis or approved portable instrumentation.

5. Details on the continuous monitors, recording devices, sample collection, calibration, monitor operating procedures, and monitor performance specification test shall be submitted for approval to the Chief - Bureau of Technical Services, Engineering and Technology Element, 380 Scotch Road, Trenton, NJ 08619.

6. The equipment in this permit shall not be used in a manner which will cause the release of any odors or smell in any area, except for those areas over which the owner or operator has exclusive use or occupancy.

7. The company is required to:

a. Conduct stack tests for the afterburner within 90 days of start-up in accordance with S.A.C. 7:27-9.4(c), for the following substances: particulates, carbon monoxide and oxygen.

b. Thirty days prior to the conduct of the required tests, submit for approval a detailed description of the sampling port locations, sampling equipment, and sampling and analytical procedures for such tests to the Chief - Bureau of Technical Services.

c. Advise the Bureau of Technical Services at 609-520-4084 and the Metropolitan Regional Field Office at 201-669-3935 at least 72 hours prior to the actual testing, in order that representatives of these offices may be scheduled to observe the conduct of the tests.

8. After receipt of the report of the stack test results, the Department shall establish maximum hourly concentrations of carbon monoxide corrected to seven percent oxygen which relate to the maximum allowable emission rates.

DIVISION OF ENVIRONMENTAL QUALITY
AIR POLLUTION CONTROL PROGRAM

All Correspondence must indicate your APC PLANT ID NUMBER

Certificate Number 082002 LBG NUMBER 862168A APC PLANT ID 10082

(Mailing Address)

MAXWELL HOUSE COFFEE DIV GENERAL FOODS
1125 HUDSON STREET
HOBOKEN NJ 07030

(Plant Location)

MAXWELL HOUSE HOBOKEN
1125 HUDSON STREET
HOBOKEN

Applicant's Designation of Equipment

AFTERBURNER STACK-Bldg #10

N.J. Stack No. 068

No. of Stacks 003

No. of Stacks 02

Approval 02/29/88

Effective 02/29/88

Expiration 05/27/88

PERMIT TO CONSTRUCT, INSTALL OR ALTER CONTROL APPARATUS OR EQUIPMENT
AND
TEMPORARY CERTIFICATE TO OPERATE CONTROL APPARATUS OR EQUIPMENT

* CONDITIONAL *

THIS PERMIT AND TEMPORARY CERTIFICATE IS BEING ISSUED UNDER THE AUTHORITY OF CHAPTER 106, P.L. 1967 (N.J.S.A.26:2C-9.2). THE TEMPORARY CERTIFICATE WILL ALLOW FOR INSPECTION AND EVALUATION TO ASSURE CONFORMANCE WITH ALL PROVISIONS OF THE NEW JERSEY ADMINISTRATIVE CODE, TITLE 7, CHAPTER 27. BASED ON THIS EVALUATION, STACK TESTS MAY BE REQUIRED IN ACCORDANCE WITH N.J.A.C. 7:27-8.4(C).

IF THE DEPARTMENT IS SOLELY RESPONSIBLE FOR BEING UNABLE TO INSPECT THIS EQUIPMENT IN OPERATION AS PERMITTED DURING THIS 90-DAY PERIOD, THIS TEMPORARY CERTIFICATE WILL BE EXTENDED AUTOMATICALLY. HOWEVER, IF YOU ARE RESPONSIBLE FOR THE DEPARTMENT'S BEING UNABLE TO INSPECT, E.G., NOT NOTIFYING THE DEPARTMENT WHEN THIS EQUIPMENT OR PROCESS IS IN OPERATION, THIS CERTIFICATE MAY NOT BE EXTENDED AND YOU WILL BE NOTIFIED BY THE DEPARTMENT THAT YOU MUST APPLY FOR AND OBTAIN AN EXTENSION AUTHORIZING YOU TO CONTINUE TO OPERATE THE EQUIPMENT. THE DEPARTMENT RESERVES THE RIGHT TO WITHHOLD ANY EXTENSION OF THIS TEMPORARY CERTIFICATE, IN WHICH EVENT YOU WILL BE NOTIFIED THAT YOU MUST APPLY FOR AND OBTAIN AN EXTENSION AUTHORIZING YOU TO CONTINUE TO OPERATE AFTER THE EXPIRATION DATE OF THIS CERTIFICATE.

IN ACCORDANCE WITH N.J.A.C. 7:27-8.3(D), THIS PERMIT AND CERTIFICATE MUST BE READILY AVAILABLE FOR INSPECTION ON THE OPERATING PREMISES.

THE FOLLOWING CONDITION(S) APPLY TO THIS PERMIT AND CERTIFICATE:

(SEE ATTACHED)

N.J. Department of Environmental Protection
Division of Environmental Quality
CN-027, 401 East State Street
Trenton, New Jersey 08625

Approved by: 

CALIBRATION DATATest Equipment CalibrationData Sheets Follow

CON SYSTEMS, INC.

Route 202 North, P.O. Box 460
THREE BRIDGES, NEW JERSEY 08887
(201) 782-5900

Meter Orifice Calibration Form (L-32)

Meter Box No. 4

Barometric Pressure (Pb) - 30.23" Hg

Calibrated by: CD Russell

Date: DEC. 15, 88

Dry Gas Meter No. 175 176 Ambient Temperature (Tamb) 70°F

ΔH	Meter Temperature (Tm)		Meter Reading (V.m)		Time @ seconds	ΔH @	ΔH Error
	Inlet (°F)	Outlet (°F)	Avg (°F)	Initial (ft³)			
Orifice Setting							
0.25	80	72	76	536	0.542	1.93	-0.1
0.50	81	71	76	536	0.759	1.97	-0.1
0.75	80	71	76	536	0.921	2.01	+0.1
1.00	80	70	75	535	1.063	2.00	0.0
1.50	78	69	74	534	1.298	2.01	+0.1
2.00	78	68	73	533	1.492	2.02	+0.1
2.50	77	67	72	532	1.671	2.01	+0.1
3.00	75	66	70	530		2.01	+0.1
Calculation					Avg.	2.00	0.0

$$\Delta H @ = \frac{0.0317 (\Delta H)}{Pb \cdot (T_{amb} + 460)} \times \left[\frac{(T_m + 460) (\Delta H @)}{(\dot{V}_m) (Y\text{-factor}) (60)} \right]$$

Note: Difference From ΔH @ not to exceed ± 0.15

Y Factor - Dry Gas Meter Correction Factor

STATE METER SHOP

0 036

PROOF AND DIFFERENTIAL TEST RECORD

Meter Size 3-175-S
~~1-130-S~~
~~1-170-S~~ Date Received JUNE 1, 1988 Inspector J. Soprano
 Date Tested 6-14-88 New Repaired ✓ Manufacturer Rohrbaugh + Assoc.
 Prover No. 1264 Temperatures: Room Air 83 F.
 Total Meters this Page 3 Oil 83 F.
 Prover Air 83 F.

Temp. Comp. Meters: $\frac{\text{Abs. Base Temp.}}{\text{Abs. Prover Temp.}} \times \text{Uncorr. \% Proof} = \text{Corr. \% Proof}$

Meter No.	Repair Class	Percent Proof		Differential Maximum	Remarks
		Check	Open		
175176	TEST	101.7	101.9	34	Uncorr. AS % Proof FOUND
					Corr. % Proof
591355	TEST	106.0	105.0	50	Uncorr. AS % Proof FOUND
					Corr. % Proof
625432	TEST	102.0	102.8	39	Uncorr. AS % Proof FOUND
					Corr. % Proof
					Uncorr. % Proof
					Corr. % Proof
175176	ADJUST	100.3	100.0	34	Uncorr. AS % Proof CALIBRATED
					Corr. % Proof
591355	ADJUST	100.2	100.2	50	Uncorr. AS % Proof CALIBRATED
					Corr. % Proof
625432	ADJUST	100.0	99.8	39	Uncorr. AS % Proof CALIBRATED
					Corr. % Proof

METER BOX I.D. T #3 METER NO. 38949 DATE INSTALLED JAN. 18, 88 BY: OBR
 BARO. PRESS. - 29.92

ΔH OFFICE SETTING	METER TEMP.		METER		TIME @ 120 sec.	ΔH @	DIFFERENCE FROM AVG. ΔH.
	IN	OUT	READING	TEMP.			
.5	84	70	537	77	120	2.04	-0.07
1.0	85	71	538	78	120	1.96	-0.15
1.5	88	72	540	80	120	1.99	-0.12
2.0	88	74	541	81	120	1.98	-0.13
2.5	84	76	540	80	120	2.26	+0.15
3.0	92	76	544	84	120	2.23	+0.12
					AVG = 2.11		

CALCULATION:

$$\Delta H @ = \frac{0.0317(\Delta H)}{29.92(1 + 4\alpha)} \left[\frac{T + 400(100)}{A(60)} \right]$$

LEAK CHECK = 0.000 CFM @ 2.8" H₂O

Box #3, METER # 38949
 CALIBRATED: SEPT. 287 by PSFG
 INSTALLED: JAN. 18, 88 by OBR
 LEAK CHECK: 0.000 CFM @ 2.8" H₂O
 REMOVED MAR. 1, 89
 ΔH @ = 2.11

NOT TO EXCEED
 F. 15 FROM AVG. ΔH @

PROOF AND DIFFERENTIAL TEST RECORD

0 038

Meter Size S-130 S-90 Date Received 8-27-87 Inspector J. SOPRANO
 Date Tested 9-2-87 New Repaired ✓ Manufacturer Rockwell + Assoc
 Prover No. 1264 Temperatures: Room Air 79 F.
 Total Meters this Page 3 011 79 F.
 Prover Air 79 F.

Temp. Comp. Meters: $\frac{\text{Abs. Base Temp.}}{\text{Abs. Prover Temp.}} \times \text{Uncorr. \% Proof} = \text{Corr. \% Proof}$

Meter No.	Repair Class	Percent Proof		Differential Maximum	Remarks
		Check	Open		
716691	INTST	99.8	100.7	20	Uncorr. $\frac{1}{2}$ Proof AS FOUND
					Corr. $\frac{1}{2}$ Proof
38949	INTST	106.2	103.8	36	Uncorr. $\frac{1}{2}$ Proof AS FOUND
					Corr. $\frac{1}{2}$ Proof
175176	INTST	98.8	98.8	28	Uncorr. $\frac{1}{2}$ Proof AS FOUND
					Corr. $\frac{1}{2}$ Proof
					Uncorr. $\frac{1}{2}$ Proof
					Corr. $\frac{1}{2}$ Proof
716691	ADJUST	100.0	100.2	20	Uncorr. AS $\frac{1}{2}$ Proof CALIBRATED
					Corr. $\frac{1}{2}$ Proof
38949	VALUE	100.0	100.1	36	Uncorr. AS $\frac{1}{2}$ Proof CALIBRATED
					Corr. $\frac{1}{2}$ Proof
175176	ADJUST	100.2	100.2	28	Uncorr. AS $\frac{1}{2}$ Proof CALIBRATED
					Corr. $\frac{1}{2}$ Proof

Date 1-2-77

Calibrated by J. J. [signature]

Nozzle identification number	Nozzle Diameter ^a			ΔD mm (in.)	D_{avg} ^c mm (in.)
	D_1 mm (in.)	D_2 mm (in.)	D_3 mm (in.)		
# 6	.500	.501	.500	.001	.500
# 10	.449	.494	.497	.001	.494
# 11	.508	.501	.502	.001	.502
# 33	.177	.176	.177	.001	.177
# 41	.500	.500	.498	.002	.499
# 42	.495	.496	.495	.001	.495
# 43	.430	.432	.431	.002	.431
# 44	.425	.425	.425	.000	.425
# 45	.425	.426	.425	.001	.425
# 46	.432	.431	.432	.001	.432
# 3	.252	.253	.252	.001	.252
# 47	.146	.146	.147	.001	.146
# 26	.187	.188	.188	.001	.188
# 18	.237	.237	.237	.000	.237

where:

^a $D_{1,2,3}$ = three different nozzles diameters, mm (in.); each diameter must be within (0.025 mm) 0.001 in.

^b ΔD = maximum difference between any two diameters, mm (in.),
 $\Delta D \leq (0.10 \text{ mm}) 0.004 \text{ in.}$

^c D_{avg} = average of D_1 , D_2 , and D_3 .

N	D-1	D-2	D-3	ΔD	avg
E10	.243	.242	.243	.001	.243

Date 12/24/87 Thermocouple number 40
 Ambient temperature 24 °C Barometric pressure 30.46 in. Hg
 Calibrator TPS Reference: mercury-in-glass ASTM
 other _____

Reference point number	Source ^a (specify)	Reference thermometer temperature, °C	Thermocouple potentiometer temperature, °C	Temperature difference, % ^b
0°	ICE WATER	0.0	0.2	0.1
100°	boiling WATER	100	99.8	0.0
—	boiling cooking oil			

^aType of calibration system used.

^b
$$\left[\frac{(\text{ref temp, } ^\circ\text{C} + 273) - (\text{test thermom temp, } ^\circ\text{C} + 273)}{\text{ref temp, } ^\circ\text{C} + 273} \right] 100 \leq 1.5\%$$

Figure 2.5 Stack temperature sensor calibration data form.

Date 12/24/87 Thermocouple number 43
Ambient temperature 24 °C Barometric pressure 30.46 in. Hg
Calibrator TPB Reference: mercury-in-glass ASTM
other _____

Reference point number	Source ^a (specify)	Reference thermometer temperature, °C	Thermocouple potentiometer temperature, °C	Temperature difference, °C ^b
0°	ICE WATER	0.0	0.3	0.2
100°	boiling WATER	100.0	100.5	0.0
—	boiling cooking oil			

^aType of calibration system used.

^b
$$\left[\frac{(\text{ref temp, } ^\circ\text{C} + 273) - (\text{test thermom temp, } ^\circ\text{C} + 273)}{\text{ref temp, } ^\circ\text{C} + 273} \right] 100 < 1.5\%$$

Figure 2.5 Stack temperature sensor calibration data form.

Date 12/24/87 Thermocouple number 46
Ambient temperature 24 °C Barometric pressure 30.46 in. Hg
Calibrator TPB Reference: mercury-in-glass ASTM
other _____

Reference point number	Source ^a (specify)	Reference thermometer temperature, °C	Thermocouple potentiometer temperature, °C	Temperature difference, ^b %
0°	ICE WATER	0.0	-0.2	0.1
100°	boiling WATER	100.0	100.6	0.2
—	boiling cooking oil			

^aType of calibration system used.

^b
$$\left[\frac{(\text{ref temp, } ^\circ\text{C} + 273) - (\text{test thermom temp, } ^\circ\text{C} + 273)}{\text{ref temp, } ^\circ\text{C} + 273} \right] 100 \leq 1.5\%$$

Figure 2.5 Stack temperature sensor calibration data form.

Date 12/24/87 Thermocouple number 41
Ambient temperature 24 °C Barometric pressure 30.46 in. Hg
Calibrator TPO Reference: mercury-in-glass ASTM
other _____

Reference point number	Source ^a (specify)	Reference thermometer temperature, °C	Thermocouple potentiometer temperature, °C	Temperature difference, % ^b
0°	ICE WATER	0.0	0.1	0.1
100°	boiling WATER	100	100.2	0.0
—	boiling cooking oil			

^aType of calibration system used.

^b
$$\left[\frac{(\text{ref temp, } ^\circ\text{C} + 273) - (\text{test thermom temp, } ^\circ\text{C} + 273)}{\text{ref temp, } ^\circ\text{C} + 273} \right] 100 \leq 1.5\%$$

Figure 2.5 Stack temperature sensor calibration data form.

Date 12/24/87 Thermocouple number 38
Ambient temperature 24 °C Barometric pressure 30.46 in. Hg
Calibrator TPB Reference: mercury-in-glass ASTM,
other _____

Reference point number	Source ^a (specify)	Reference thermometer temperature, °C	Thermocouple potentiometer temperature, °C	Temperature difference, % ^b
0°	ICE WATER	0.0	0.3	0.1
100°	boiling WATER	99.5	99.2	0.0
—	boiling cooking oil			

^aType of calibration system used.

^b
$$\left[\frac{(\text{ref temp, } ^\circ\text{C} + 273) - (\text{test thermom temp, } ^\circ\text{C} + 273)}{\text{ref temp, } ^\circ\text{C} + 273} \right] \cdot 100 \leq 1.5\%$$

Figure 2.5 Stack temperature sensor calibration data form.

Date 12/28/87 Thermocouple number 5
Ambient temperature 24 °C Barometric pressure 30.25 in. Hg
Calibrator TPB Reference: mercury-in-glass ASTM
other _____

Reference point number	Source ^a (specify)	Reference thermometer temperature, °C	Thermocouple potentiometer temperature, °C	Temperature difference, % ^b
0°	ICE WATER	0.0	- 0.2	0.1
100°	boiling WATER	100.0	100.0	0.0
—	boiling cooking oil			

^aType of calibration system used.

^b
$$\left[\frac{(\text{ref temp, } ^\circ\text{C} + 273) - (\text{test thermom temp, } ^\circ\text{C} + 273)}{\text{ref temp, } ^\circ\text{C} + 273} \right] 100 \leq 1.5\%$$

Figure 2.5 Stack temperature sensor calibration data form.

PITOT TUBE CALIBRATION

Pitot tube calibration number 7 Date JAN. 20, 88
 Calibrated by BROWN & RUFF @ RSU
 EFFECTIVE LENGTH 3'

A Side Calibration

Run No.	ΔP_{std} cm H ₂ O (in. H ₂ O)	ΔP_s cm H ₂ O (in. H ₂ O)	$C_{p(s)}$	Deviation $C_{p(s)} - \bar{C}_{p(A)}$
1	0.47	0.65	0.842	+0.003
2	0.48	0.67	0.838	-0.001
3	0.48	0.67	0.838	-0.001
$\bar{C}_{p(side A)}$			0.839	$\delta = ? *$

B Side Calibration

Run No.	ΔP_{std} cm H ₂ O (in. H ₂ O)	ΔP_s cm H ₂ O (in. H ₂ O)	$C_{p(s)}$	Deviation $C_{p(s)} - \bar{C}_{p(B)}$
1	0.48	0.69	0.826	+0.005
2	0.47	0.69	0.817	-0.004
3	0.48	0.70	0.820	-0.001
$\bar{C}_{p(side B)}$			0.821	$\delta = ? *$

$$C_p(A) - C_p(B) = 0.018 *$$

Figure 4-10. Pitot tube calibration data.

* VALUE MUST BE $\leq \pm 0.01$

FORM: L-26 (REV. JUNE 10, 87)

RECON SYSTEMS, INC.
 Route 202 North P.O. Box 460
 THREE BRIDGES, NEW JERSEY 08887
 (201) 782-5900

PITOT TUBE CALIBRATION

Pitot tube calibration number 19 Date JAN. 20, 88
 Calibrated by BROWN & RUFF @ RSU
 EFFECTIVE LENGTH 4'

A Side Calibration

Run No.	ΔP_{std} cm H ₂ O (in. H ₂ O)	ΔP_s cm H ₂ O (in. H ₂ O)	$C_{p(s)}$	Deviation $C_{p(s)} - \bar{C}_{p(A)}$
1	0.48	0.68	0.832	+0.001
2	0.48	0.67	0.838	+0.007
3	0.47	0.68	0.823	-0.008
$\bar{C}_{p(side A)}$			0.831	$\delta = ? *$

B Side Calibration

Run No.	ΔP_{std} cm H ₂ O (in. H ₂ O)	ΔP_s cm H ₂ O (in. H ₂ O)	$C_{p(s)}$	Deviation $C_{p(s)} - \bar{C}_{p(B)}$
1	0.46	0.70	0.803	-0.009
2	0.47	0.69	0.817	+0.005
3	0.47	0.69	0.817	+0.005
$\bar{C}_{p(side B)}$			0.812	$\delta = ? *$

$$C_p(A) - C_p(B) = +0.019 *$$

Figure 4-10. Pitot tube calibration data.

* VALUE MUST BE $\leq \pm 0.01$

FORM: L-26 (REV. JUNE 10, 87)

RECON SYSTEMS, INC.
 Route 202 North P.O. Box 460
 THREE BRIDGES, NEW JERSEY 08887
 (201) 782-5900

ORIGINAL DATA AND CALCULATION SHEETS

PARTICULATE FIELD

DATA BOOK

0 049

DAILY
STACK/AIR
TESTING
FIELD REPORT

F-19 (7.13.88)

cc: billing _____
chron _____
Original to Job file _____

Date 2/1/89

Client Bruno Padovan

RECON Job No. 0641

Project Manager PFM

Field Supervisor PFM

Jobsite Company Maxwell House Street 1125 Hudson St.

City Hoboken State NJ Zip _____ Phone 201-525-1500

Processes, Stacks, Vents, Air etc. Tested Today

1. Afterburner Inlet Condition* _____
2. Afterburner Outlet Condition* _____
3. _____ Condition* _____
4. _____ Condition* _____

* (e.g. stack opacity, raining?, odors, color, flowrate; process steady or upset; etc.)

Milestone Times (Military)

Departure from home or RECON 0700 Arrival at site 0730 Lunch _____ to _____

Lost Time _____ to _____ Arrival at home or RECON 1530

Reason For Lost Time _____

Client or Job Site Rep Aware of Lost Time _____ yes _____ no Person _____

Personnel Onsite

RECON PFM TFM CDR TPB

Client _____

Jobsite Reps Bruno Padovan

Agency Observing (1) NIJAS (2) _____

Agency Personnel (1) Stafford Stewart Rob Tenbrevilla Mike Gasek

(2) _____

Other _____

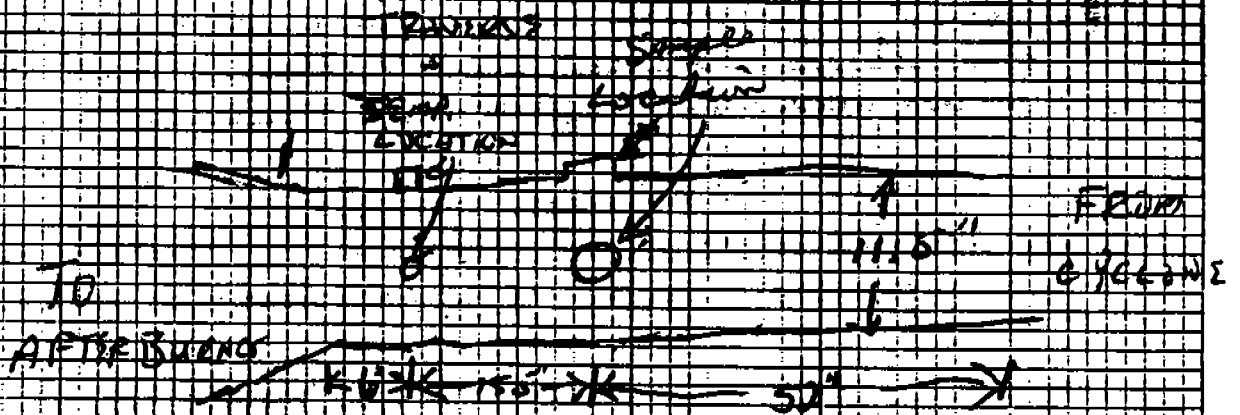
Out of Scope Work Requested and Performed

Stack and Process Sketches

0 000

Initial

VOLCANO
MISTIFIED



PROBE MARKINGS - CIRCULAR STACK

0 051

STACK ID & PORT 11.5 INCHES

PORT EXTENSION 1 1/8 INCHES

RIGHT MOST COLUMN IS THE DISTANCE FROM PROBE TIP TO OUTSIDE OF PORT EXTENSION.

EPA DISTANCE "A" _____ DIAMETERS

EPA DISTANCE "B" _____ DIAMETERS

TRAVERSE POINT NUMBER	LENGTH FACTOR FROM EPA METHOD 1 TABLE 1-2, K _L	PRODUCT OF LENGTH FACTOR TIMES STACK INSIDE DIAMETER (INCHES) K _L X (STACK ID)	SUM OF PREVIOUS COLUMN AND PORT EXTENSION (INCHES) K _L X (STACK ID) + PORT EXTENSION	CONVERT PREVIOUS COLUMN TO INCHES AND COMMON FRACTIONS
1	2.1	0.24 - 0.5	1.625	1 5/8
2	6.7	0.77	1.826	1 15/16
3	11.8	1.36	2.48	
4	17.7	2.04	3.16	
5	25.0	2.875	4.0	
6	35.6	4.04	5.22	
7	64.4	7.41	8.5	8 1/2
8	75.0	8.625	9.75	9 3/4
9	82.3	9.46	10.6	10 5/8
10	88.2	10.14	11.3	11 5/16
11	93.3	10.73	11.85	11 7/8
12	97.9	11.25 - 10.0	12.38	12 1/8

CIRCULAR STACK CROSS SECTIONAL AREA = CSA = $\frac{\pi D^2}{4}$ = $\frac{\pi (11.5)^2}{4}$ = 0.723 FT²

PROBE MARKINGS - RECTANGULAR STACK

STACK CROSS SECTION DIMENSIONS _____ INCHES

PORT EXTENSIONS _____ INCHES

TO DETERMINE UPSTREAM/DOWNSTREAM DISTURBANCES, THE EQUIVALENT DIAMETER IS DETERMINED USING THE FOLLOWING EQUATION $d_e = \frac{2LV}{L+V}$

EPA DISTANCE "A" _____ DIAMETERS

EPA DISTANCE "B" _____ DIAMETERS

TRAVERSE POINT NUMBER	CENTROID OF EACH EQUAL AREA (INCHES)	SUM OF PREVIOUS COLUMN AND PORT EXTENSION
1		
2		
3		
4		
5		
6		
7		

RECTANGULAR STACK CROSS SECTIONAL AREA = CSA = $\frac{L \times V}{144}$ = $\frac{(\text{L}) \times (\text{V})}{144}$ = _____ FT²

PRELIMINARY DATA

0 052

Cp = _____
delta H₂ = _____

% H₂O = _____
P_s = P_b + (+) P static = _____ Hg" (absolute)

Pb _____

P static = -4.4

T_s = _____ °F

% CO₂ = _____ x 0.44 = _____

T_m = _____ °F

% O₂ = _____ x 0.32 = _____

delta P (average) = _____ "H₂O

% N₂ = _____ x 0.28 = _____

Dry MW = _____

MW = 0.18 (XH₂O) + Dry MW (100 - XH₂O) / 100

Cross Sectional Area _____ ft²

MW = _____

CALCULATIONS

VELOCITY (ACTUAL) IN STACK = 85.48(Cp) $\sqrt{\frac{T_s + 460}{P_s(MW)}} \sqrt{\Delta P} = 85.48 (0.99) \sqrt{\frac{(1110)}{(29.58)(28.75)}} \sqrt{\Delta P}$

V_s = (84.62) $\sqrt{1.30 \Delta P} = (84.62)(1.14) \sqrt{\Delta P}$

V_s = (96.48) $\sqrt{\Delta P} = (96.48)(0.67) = 64.72$ FT/SEC

ACFM = (V_s)(60)(CSA) = (64.72)(60)(0.723) = 2808

VELOCITY @ Stp V_{s-std} = V_s (17.65) $\left(\frac{P_s}{T_s + 460} \right) = \frac{(64.72)(17.65)(29.58)}{(1110)} = 30.44$ FT/SEC

SCFM = (V_{s-std})(CSA)(60) = (30.44)(0.723)(60) = 1320

DSCFM = $\left(\frac{100 - XH_2O}{100} \right)$ (SCFM) = (1320)(.95) = 1254

PRELIMINARY DATA

COMPANY: MAXWELL HouseSAMPLE LOCATION: Inlet 0 053DATE: 1/31/89

TIME: _____

PITOT TUBE LINES LEAK CHECK ☒LEVEL AND ZERO MANOMETER ☒ESTIMATED MOISTURE (%) 12 C_p .99

DRY BULB (°F) _____ WET BULB (°F) _____

DIRECTION OF FLOW to afterburner

TRAVERSE POINT NUMBER	CYCLONIC FLOW ANGLE THAT YIELDS A NULL DELTA P	VELOCITY HEAD DELTA P INCHES OF H ₂ O	STACK TEMPERATURE (DEGREES F)
A 1	0.2	0.45	161
2	2	0.47	162
3	4	0.49	163
4	4	0.51	164
5	2	0.52	165
6	2	0.51	166
7	4	0.45	166
8	4	0.44	165
9	5	0.42	155
10	7	0.41	154
11	5	0.41	151
12	2	0.39	149
B 1		0.40	161
2	constant	0.42	164
3	BC	0.45	168
4	DETERMINED	0.46	170
5	in	0.47	172
6	A	0.45	174
7	HORIZONTAL	0.45	174
8	DUCT	0.46	173
9		0.47	164
10		0.47	159
11		0.45	157
12		0.43	153
AVERAGE			

AVERAGE ANGLE MUST BE <20 DEGREES

0.45

0 054

PARTICULATE FIELD DATA SHEET

PLANT Maxwell House DATE 1/31/89 RUN NO. one
 SAMPLE LOCATION Inlet RAC BOX NO. 3 DRY GAS METER NO. 38949
 NOZZLE NO. 27 NOZZLE SIZE 0.249 INCHES PITOT NO. 5 C_p .99
 TIME AT EACH POINT 60 MINUTES DELTA H 2.11 THERMOCOUPLE NO.: T 46
 AMBIENT PRESSURE (P_{BAR}) 29.91 "HG PROBE OUTLET 40
 BOX OUTLET 43
 STATIC PRESSURE (P) -4.4 "H₂O/13.6 = _____ "Hg(P meter) ΔH 4.5
 STACK PRESSURE (P_s) = P_{bar} + P_{meter} = _____ "Hg OPERATING CONDITION OR REMARKS _____
 DRY BULB _____ °F WET BULB _____ °F _____ %H₂O _____

PORT/ POINT	MILITARY CLOCK TIME	METER READING	PITOT DELTA P "H ₂ O	ORIFICE DELTA H "H ₂ O	METER TEMP. °F		LINE VAC "Hg	PROBE OUTLET °F	BOX OUTLET TEMP °F	BOX TEMP °F	STACK TEMP °F
					IN	OUT					
A1	1000	242.95	0.45	2.0	96	94	6	154	195	235	161
2	1002:30		0.47	2.1	106	96	6	184	206	270	162
3	1005		0.49	2.2	109	96	6	208	221	270	163
4	1007:30		0.51	2.3	110	98	7	229	240	255	164
5	1010		0.52	2.3	112	98	7	201	243	235	165
6	1012:30		0.51	2.3	113	98	7	211	243	210	166
7	1015		0.45	2.0	114	98	6	224	240	200	166
8	1017:30		0.44	2.0	114	98	6	212	237	190	165
9	1020		0.42	1.9	114	98	6	227	235	180	155
10	1022:30		0.41	1.85	114	100	6	211	233	175	154
11	1025		0.41	1.85	114	100	6	208	229	165	151
12	1027:30		0.39	1.75	114	100	6	227	224	160	149
	1030	265.160	STOP TEST								
B1	1115	265.160	0.40	1.8	104	96	6	189	174	310	161
2	1117:30		0.42	1.9	108	96	6	209	206	330	168
3	1120		0.45	2.0	108	96	6	226	227	345	168
4	1122:30		0.46	2.0	111	96	6	204	250	300	170
5	1125		0.47	2.1	112	98	6	180	258	270	172
6	1127:30		0.45	2.0	112	98	6	198	250	250	174
7	1130		0.45	2.0	112	100	6	212	247	225	174
8	1132:30		0.46	2.1	114	100	6	231	245	210	173
9	1135		0.47	2.1	114	100	6	206	246	200	164
10	1137:30		0.47	2.1	114	100	6	205	240	190	159
11	1140		0.45	2.0	114	100	6	225	235	150	157
12	1142:30	256.700	0.43	1.9	114	100	6	217	234	170	153
*	0 100	43.725	delta H =	T _m =						T _s =

* Sum, average or Difference

Pre-Leak Check 0.005 @ 15"Post Leak Check 0.001 @ 7"

FYRITE:

% OXYGEN

20.5

% CARBON DIOXIDE

0.5

CLIENT: HANCOCK HOUSE
 SAMPLING DATE: 1/31/89
 SAMPLING TIME: 1000-1140
 UNIT SAMPLED: UNIT 1

Date: 02/06/89
 Time: 10:00 AM
 Run # 1

AVERAGE VELOCITY PRESSURE

Delta P (IN H ₂ O)	Delta P Square Root
0.40	0.67
0.47	0.69
0.49	0.70
0.51	0.71
0.52	0.72
0.51	0.71
0.45	0.67
0.44	0.66
0.42	0.65
0.41	0.64
0.41	0.64
0.39	0.62
0.40	0.63
0.42	0.65
0.40	0.67
0.46	0.68
0.47	0.69
0.43	0.67
0.43	0.67
0.46	0.68
0.47	0.69
0.47	0.69
0.45	0.67
0.43	0.66

THE AVERAGE SQUARE ROOT OF DELTA P = 0.6717101

0 056

CLIENT: MAWELL HOUSE
 SAMPLING DATE: 1/31/89
 SAMPLING TIME: 1000-1145
 UNIT SAMPLED: INLET

Date: 02/26/89
 Time: 10:34 AM
 Run # 1

Delta H (IN H ₂ O)	Meter Temp (F)		Stack Temp (F)
	IN	OUT	
2.00	96.00	94.00	161.00
2.10	106.00	96.00	162.00
2.20	109.00	98.00	163.00
2.30	110.00	98.00	164.00
2.40	112.00	98.00	165.00
2.50	113.00	98.00	166.00
2.60	114.00	98.00	166.00
2.70	114.00	98.00	165.00
1.70	114.00	98.00	165.00
1.80	114.00	100.00	154.00
1.90	114.00	100.00	151.00
1.72	114.00	100.00	149.00
1.60	104.00	96.00	161.00
1.70	108.00	96.00	164.00
2.00	108.00	96.00	168.00
2.10	111.00	96.00	170.00
2.10	112.00	98.00	172.00
2.00	112.00	98.00	174.00
2.00	112.00	100.00	174.00
2.10	114.00	100.00	173.00
2.10	114.00	100.00	164.00
2.10	114.00	100.00	159.00
2.00	114.00	100.00	157.00
1.70	114.00	100.00	153.00

AVERAGES

DELTA H = 2.02/083 IN H₂O
 METER TEMP. = 104.6042 F
 STACK TEMP. = 162.9167 F

SAMPLE LOCATION WINDY INLET

MOISTURE DETERMINATION

RUN NO. 1

DATE 1/31/89

0 051

CHAIN-OF-CUSTODY SAMPLE NO. _____

GRAMS

IMPINGER 1 FINAL WEIGHT 797.7
INITIAL WEIGHT 749.0
INCREASE

IMPINGER 2 FINAL WEIGHT 735.5
INITIAL WEIGHT 705.0
INCREASE

IMPINGER 3 FINAL WEIGHT 491.1
INITIAL WEIGHT 488.3
INCREASE

SILICA GEL FINAL WEIGHT 741.7
INITIAL WEIGHT 728.9
INCREASE

GRAMS

IMPINGER 1 48.7

IMPINGER 2 30.5

IMPINGER 3 2.8

SILICA GEL 12.8

TOTAL MASS OF WATER CAUGHT 94.8 GRAMS

CHAIN-OF-CUSTODY SAMPLE NO. _____

FILTER DIAMETER 4 INCHES

FILTER TYPE Glass Fiber

FILTER: FINAL WEIGHT .6855 GMS
INITIAL WEIGHT .6268 GMS
INCREASE

.0587 GRAMS

TOTAL MASS OF PARTICULATE CAUGHT THIS FILTER

IS ICE PRESENT IN THE IMPINGER BATH AT THE END OF THIS SAMPLE? YES _____ NO _____

CALCULATIONS

$$V_{m-std} = 17.65 (V_m) \left(\frac{P_{bar} + \Delta H / 13.6}{T_m + 460} \right) = 17.65 () \left(\frac{+ 13.6}{+ 460} \right)$$

$$= 17.65 () () = \text{_____} \text{ FT}^3$$

$$V_{w-std} (H_2O) = \frac{\text{GRAMS COLLECTED}}{21.2 \text{ GRAMS/FT}^3} = \frac{()}{(21.2)} = \text{_____} \text{ FT}^3$$

$$\% H_2O = \frac{(V_{w-std}) 100}{((V_{m-std}) + (V_{w-std}))} = \frac{100 ()}{() + ()} = \frac{()}{()} = \text{_____} \%$$

$$\text{MOLECULAR WEIGHT (MW)} = \frac{18 (XH_2O)}{100} + \frac{\text{DRY MW} (100 - XH_2O)}{100} = 0.18 () + \frac{() ()}{100}$$

$$\text{VELOCITY (ACTUAL) IN STACK} = 85.48 (C_p) \sqrt{\frac{T_s + 460}{P_s (MW)}} \sqrt{\Delta P} = 85.48 () \sqrt{\frac{()}{() ()}} \sqrt{\Delta P}$$

$$V_s = () \sqrt{\Delta P} = () () \sqrt{\Delta P}$$

$$V_s = () \Delta P = () () = \text{_____} \text{ FT/SEC}$$

$$\text{ACFM} = (V_s) (60) (CSA) = () (60) () = \text{_____}$$

$$\text{VELOCITY @ Stp } V_{s-std} = V_s (17.65) \left(\frac{P_s}{T_s + 460} \right) = \frac{() (17.65) ()}{()} = \text{_____} \text{ FT/SEC}$$

$$\text{SCFM} = (V_{s-std}) (CSA) (60) = () () (60) = \text{_____}$$

$$\text{DSCFM} = \left(\frac{100 - XH_2O}{100} \right) (\text{SCFM}) = () () = \text{_____}$$

$$\text{NOZZLE VELOCITY @ STD } V_n = \frac{(V_{m-std} + V_{w-std})}{60 (0) A_n} = \frac{()}{60 () () (10^{-4})} = \text{_____} \text{ FT/SEC}$$

$$I = \frac{100 V_{n-std}}{V_{s-std}} = \frac{100 ()}{()} = \text{_____} \% \text{ Isokinetic}$$

0 058

LAB DATA - EVAPORATIONS

PLANT Maxwell House
 SAMPLING DATE 1/31/89
 CHAIN-OF-CUSTODY SAMPLE NO. _____

SAMPLE LOCATION Inlet RUN NO. 1 FOR _____
 OPERATING CONDITION _____

ACETONE WASHINGS

GROSS 646.8 GMS
 TOTAL TARE - 457.3 GMS
 SAMPLE (A) NET 189.5 GMS
 AMOUNT EVAPORATED (B) 189.5 GMS
 EVAP. BEAKER NO. _____
 GROSS 103.1418 GMS
 TARE - 102.1060 GMS
 (C) NET 0.0358 GMS

ACETONE BLANK

EVAP. BEAKER NO. _____
 GROSS 99.6314 GMS
 TARE - 99.6316 GMS
 NET 0 GMS

ACETONE BLANK = NET 100 GMS (D)
 TOTAL AMOUNT EVAPORATED 100 GMS (F)

CORRECTED NET (E) = (C) - (B) $\left[\frac{(D)}{(F)} \right]$
 = 0.0358 - 189.5 $\left[\frac{100}{189.5} \right]$
 = 0.0358 GMS (E) = (C) - B $\left[\frac{(D)}{(F)} \right]$

SCALED UP NET = (E) $\left(\frac{A}{B} \right)$
 = 0 $\left(\frac{189.5}{189.5} \right)$
 = 0.0358

VET CATCH

GROSS _____ GMS
 TOTAL TARE - _____ GMS
 SAMPLE (A) NET _____ GMS
 AMOUNT EXTRACTED (G) _____ GMS (MLS)
 AMOUNT OF E/C _____ GMS (H)

WATER PHASE EVAP. BEAKER NO. _____

GROSS _____ GMS
 TARE - _____ GMS
 (J) NET _____ GMS
 WATER BLANK (L) = _____ GMS
 100 GMS

CORRECTED NET (N) = J - (G)(L)
 = _____ $\left(\frac{100}{100} \right)$
 = _____ GMS

SCALED UP NET = (N) $\left(\frac{E}{G} \right)$
 = _____ $\left(\frac{189.5}{189.5} \right)$
 = _____ GMS

EC PHASE EVAP. BEAKER NO. _____

GROSS _____ GMS
 TARE - _____ GMS
 (K) NET _____ GMS
 E/C BLANK (M) = _____ GMS
 100 MLS

CORRECTED NET (N) = K - (H)(M)
 = _____ $\left(\frac{100}{100} \right)$
 = _____ GMS

SCALED UP NET = (P) $\left(\frac{E}{G} \right)$
 = _____ $\left(\frac{189.5}{189.5} \right)$
 = _____ GMS

D# 4.9

PARTICULATE FIELD DATA SHEET

PLANT Maxwell HouseDATE 2/1/89RUN NO. 2 0 000SAMPLE LOCATION InletRAC BOX NO. 3DRY GAS METER NO. 38949NOZZLE NO. 27 NOZZLE SIZE 0.249 INCHESPITOT NO. 5C_p 0.99TIME AT EACH POINT (Ø) 60 MINUTESDELTA H Ø 2.11THERMOCOUPLE NO.: T 46AMBIENT PRESSURE (P_{BAR}) 29.78 "HGPROBE OUTLET 40BOX OUTLET 43STATIC PRESSURE (P) -4.3 "H₂O/13.6 = -0.316 "Hg(P meter)STACK PRESSURE (P_s) = P_{bar} + P_{meter} = _____ "Hg OPERATING CONDITION OR REMARKS _____DRY BULB _____ °F WET BULB _____ °F _____ "H₂O

PORT/ POINT	MILITARY CLOCK TIME	METER READING	PITOT DELTA P "H ₂ O	ORIFICE DELTA H "H ₂ O	METER TEMP. °F		LINE VAC "Hg	PROBE OUTLET °F	BOX OUTLET TEMP °F	BOX TEMP °F	STACK TEMP °F
					IN	OUT					
1	0802	309.009	0.56	2.7	92	88	9	173	170	300	184
2	0804:30		0.56	2.7	96	88	10	202	198	250	189
3	0807		0.58	2.8	101	90	11	220	219	250	193
4	0809:30		0.60	2.9	106	90	11	236	233	250	194
5	0812		0.58	2.8	109	90	11	219	243	210	195
6	0814:30		0.56	2.7	112	92	11	216	241	200	196
7	0817		0.51	2.5	114	92	10	232	237	185	195
8	0819:30		0.48	2.4	114	94	10	219	239	175	184
9	0822		0.47	2.3	115	96	9	227	233	175	179
10	0824:30		0.47	2.3	115	96	9	217	231	165	177
11	0827		0.44	2.15	116	98	9	227	227	160	175
12	0828:30	33.595	0.42	2.05	116	100	8	203	224	160	173
B1	0858	33.671	0.50	2.55	105	98	9	143	154	210	195
2	0852:30		0.52	2.5	108	100	9	173	173	230	200
3	0856		0.54	2.65	112	100	9	210	204	250	203
4	0858:30		0.54	2.65	112	100	9	228	232	250	206
5	0901		0.54	2.65	116	102	9	240	240	250	209
6	0903:30		0.53	2.6	118	102	10	217	240	250	210
7	0906		0.51	2.5	112	102	10	204	240	250	210
8	0908:30		0.49	2.45	116	102	10	182	230	250	203
9	0911		0.50	2.45	118	102	10	194	216	250	201
10	0913:30		0.46	2.25	119	100	9	211	213	250	198
11	0916		0.29	1.3	118	102	9	217	215	250	196
12	0918:30		0.34	1.25							192
	0921	356.25									
*	Ø	V=49.759	delta H =	T _m =						T _s =

* Sum, average or Difference

Pre-Leak Check 0.005 @ 15"Post Leak Check 0.008 @ 15"FYRITE: % OXYGEN 20.0
% CARBON DIOXIDE 0.0

PARTICULATE.ATG (August 1988)

AirRecon
THREE BRIDGES, NJ

DATE: 11/11/76
 TIME: 10:34 AM
 RUN # 2
 SAMPLE TIME: 0.001072
 UNIT SAMPLED: INLET

Date: 11/11/76
 Time: 10:34 AM
 Run # 2

AVERAGE VELOCITY PRESSURE

Delta P
 (IN H2O) Delta P
 Square Root

0.56	0.75
0.56	0.75
0.56	0.76
0.60	0.77
0.58	0.76
0.56	0.75
0.53	0.71
0.48	0.69
0.47	0.67
0.47	0.67
0.44	0.66
0.42	0.65
0.50	0.71
0.52	0.72
0.54	0.73
0.54	0.73
0.54	0.73
0.53	0.73
0.51	0.71
0.47	0.70
0.50	0.71
0.46	0.68
0.29	0.54
0.36	0.60

THE AVERAGE SQUARE ROOT OF DELTA P = .7054586

0 082

CLIENT: HAWELL MOUSE
 SAMPLING DATE: 2/17/89
 SAMPLING TIME: 0802-0921
 UNIT SAMPLED: 1000

Date: 02/17/89
 Time: 10:34 AM
 Run # 2

Delta H IN H2O	Meter Temp (F) IN	Stack Temp (F) OUT	
2.70	92.00	88.00	184.00
2.70	96.00	88.00	189.00
2.80	101.00	90.00	193.00
2.90	106.00	90.00	194.00
2.80	109.00	90.00	195.00
2.70	112.00	92.00	196.00
2.50	114.00	92.00	195.00
2.40	114.00	94.00	184.00
2.30	115.00	95.00	179.00
2.30	115.00	95.00	177.00
2.15	116.00	98.00	175.00
2.05	116.00	100.00	173.00
2.00	105.00	98.00	195.00
2.50	108.00	100.00	200.00
2.65	112.00	100.00	203.00
2.65	112.00	100.00	206.00
2.65	116.00	102.00	207.00
2.60	116.00	102.00	210.00
2.50	116.00	102.00	210.00
2.45	116.00	102.00	203.00
2.40	116.00	102.00	201.00
2.20	117.00	106.00	196.00
1.50	116.00	101.00	196.00
1.75	116.00	102.00	192.00

AVERAGES

DEL H2O 2.438200 IN H2O

METER 104.375 F

STACK 191.125 F

MOISTURE DETERMINATION

0 063

SAMPLE LOCATION INLET.

RUN NO. 2

DATE 2/1/89

CHAIN-OF-CUSTODY SAMPLE NO. _____

		GRAMS
IMPINGER 1	FINAL WEIGHT	<u>781.8</u>
	INITIAL WEIGHT	<u>735.9</u>
	INCREASE	
IMPINGER 2	FINAL WEIGHT	<u>739.6</u>
	INITIAL WEIGHT	<u>715.9</u>
	INCREASE	
IMPINGER 3	FINAL WEIGHT	<u>504.7</u>
	INITIAL WEIGHT	<u>500.5</u>
	INCREASE	
SILICA GEL	FINAL WEIGHT	<u>844.8</u>
	INITIAL WEIGHT	<u>825.0</u>
	INCREASE	

	GRAMS
IMPINGER 1	<u>45.9</u>
IMPINGER 2	<u>23.7</u>
IMPINGER 3	<u>4.2</u>
SILICA GEL	<u>19.8</u>

TOTAL MASS OF WATER CAUGHT

93.6 GRAMS

CHAIN-OF-CUSTODY SAMPLE NO. _____

FILTER DIAMETER 4 INCHES

FILTER TYPE Class. Fth

FILTER: FINAL WEIGHT .7033 GMS
INITIAL WEIGHT .6292 GMS
INCREASE

.0741 GRAMS

TOTAL MASS OF PARTICULATE CAUGHT THIS FILTER

IS ICE PRESENT IN THE IMPINGER BATH AT THE END OF THIS SAMPLE? YES _____ NO _____

CALCULATIONS

$$V_{m-std} = 17.65 (V_m) \left(\frac{P_{bar} + \Delta H / 13.6}{T_m + 460} \right) = 17.65 () \left(\frac{ + 13.6 }{ } \right)$$

$$= 17.65 () () = \text{_____} \text{ FT}^3$$

$$V_{w-std} (H_2O) = \frac{\text{GRAMS COLLECTED}}{21.2 \text{ GRAMS/FT}^3} = \frac{()}{(21.2)} = \text{_____} \text{ FT}^3$$

$$X_{H_2O} = \frac{(V_{w-std}) 100}{((V_{m-std}) + (V_{w-std}))} = \frac{100 ()}{() + ()} = \frac{()}{()} = \text{_____} \%$$

$$\text{MOLECULAR WEIGHT (MW)} = \frac{18 (X_{H_2O})}{100} + \text{DRY MW} \left(\frac{100 - X_{H_2O}}{100} \right) = 0.18 () + \frac{() ()}{100}$$

$$\text{VELOCITY (ACTUAL) IN STACK} = 85.48 (C_p) \sqrt{\frac{T_s + 460}{P_s (MW)}} \sqrt{\Delta P} = 85.48 () \sqrt{\frac{()}{() ()}} \sqrt{\Delta P}$$

$$V_s = () \sqrt{\Delta P} = () () \sqrt{\Delta P}$$

$$V_s = () \Delta P = () () = \text{_____} \text{ FT/SEC}$$

$$\text{ACFM} = (V_s) (60) (CSA) = () (60) () = \text{_____}$$

$$\text{VELOCITY @ Std } V_{s-std} = V_s (17.65) \left(\frac{P_s}{T_s + 460} \right) = \frac{() (17.65) ()}{()} = \text{_____} \text{ FT/SEC}$$

$$\text{SCFM} = (V_{s-std}) (CSA) (60) = () () (60) = \text{_____}$$

$$\text{DSCFM} = \left(\frac{100 - X_{H_2O}}{100} \right) (\text{SCFM}) = () () = \text{_____}$$

$$\text{NOZZLE VELOCITY @ STD } V_n = \frac{(V_{m-std} + V_{w-std})}{60 (0) A_n} = \frac{()}{60 () () (10^{-4})} = \text{_____} \text{ FT/SEC}$$

$$I = \frac{100 V_{n-std}}{V_{s-std}} = \frac{100 ()}{()} = \text{_____} \% \text{ Isokinetic}$$

LAB DATA - EVAPORATIONS

0 084

PLANT MAXWELL House

SAMPLE LOCATION Inlet

RUN NO. 2 FOR

SAMPLING DATE 2-1-89

OPERATING CONDITION

CHAIN-OF-CUSTODY SAMPLE NO.

ACETONE WASHINGS

GROSS 661.4 GMS
TOTAL SAMPLE TARE - 456.8 GMS
(A) NET 204.6 GMS
AMOUNT EVAPORATED (B) 204.6 GMS
EVAP. BEAKER NO. _____
GROSS 110.5458 GMS
TARE - 110.4860 GMS
(C) NET 0.0598 GMS

ACETONE BLANK

EVAP. BEAKER NO. _____
99.6314 GROSS 110.5458 GMS
99.6316 TARE - 110.4860 GMS
0 NET 0.0598 GMS

ACETONE BLANK = NET 100 GMS (D)
TOTAL AMOUNT EVAPORATED 100 GMS (F)

CORRECTED NET (E) = (C) - (B) $\left[\frac{(D)}{(F)} \right]$
= 0.0598 - 204.6 $\left[\frac{100}{100} \right]$
= 0.0598 GMS

SCALED UP NET = (E) $\left(\frac{A}{B} \right)$
= 0.0598 $\left(\frac{204.6}{204.6} \right)$
= 0.0598

WET CATCH

GROSS _____ GMS
TOTAL SAMPLE TARE - _____ GMS
(A) NET _____ GMS
AMOUNT EXTRACTED (G) _____ GMS (HLS)
AMOUNT OF E/C _____ GMS (H)

WATER PHASE
EVAP. BEAKER NO. _____
GROSS _____ GMS
TARE - _____ GMS
(J) NET _____ GMS
WATER BLANK
(L) = 100 GMS

CORRECTED NET
(N) = J - (G)(L)
= _____ $\left(\frac{100}{100} \right)$
= _____ GMS
SCALED UP NET = (N) $\left(\frac{E}{G} \right)$
= _____ $\left(\frac{100}{100} \right)$
= _____ GMS

EC PHASE
EVAP. BEAKER NO. _____
GROSS _____ GMS
TARE - _____ GMS
(K) NET _____ GMS
E/C BLANK
(M) = 100 HLS

CORRECTED NET
(P) = K - (N)(M)
= _____ $\left(\frac{100}{100} \right)$
= _____ GMS
SCALED UP NET = (P) $\left(\frac{E}{G} \right)$
= _____ $\left(\frac{100}{100} \right)$
= _____ GMS

$\Delta H = 4.9$

0 066

PARTICULATE FIELD DATA SHEET

PLANT MAYWELL HOUSEDATE 2/1/89RUN NO. 3SAMPLE LOCATION InletRAC BOX NO. 3DRY GAS METER NO. 38949NOZZLE NO. 27 NOZZLE SIZE 0.249 INCHESPITOT NO. 5C_p 0.99TIME AT EACH POINT (S) 60 MINUTESDELTA H 2.11THERMOCOUPLE NO.: T₁ 46AMBIENT PRESSURE (P_{BAR}) 29.80 "HGPROBE OUTLET₁ 46BOX OUTLET 43STATIC PRESSURE (P) -4.2 "H₂O/13.6 = _____ "Hg (P meter)STACK PRESSURE (P_s) = P_{bar} + P_{meter} = _____ "Hg OPERATING CONDITION OR REMARKS _____DRY BULB _____ °F WET BULB _____ °F _____ "H₂O

PORT/ POINT	MILITARY CLOCK TIME	METER READING	PITOT DELTA P "H ₂ O	ORIFICE DELTA H "H ₂ O	METER TEMP. °F		LINE VAC "Hg	PROBE OUTLET °F	BOX OUTLET TEMP °F	BOX TEMP °F	STACK TEMP °F
					IN	OUT					
A-1	10:48	357.081	0.49	2.4	88	88	8	98	216	245	195
2	1049:30		0.47	2.3	90	88	8	139	242	240	197
3	1052		0.56	2.7	94	88	9	183	247	230	198
4	1054:30		0.59	2.9	99	90	8	202	251	220	199
5	1057		0.58	2.85	102	90	9	220	252	220	200
6	1059:30		0.58	2.85	104	92	9	227	248	210	201
7	1102		0.55	2.7	105	92	9	230	247	210	202
8	1104:30		0.49	2.4	106	92	8	220	210	210	201
9	1107		0.48	2.35	108	92	8	210	199	200	199
10	1109:30		0.36	1.75	111	94	7	204	221	190	194
11	1112		0.38	1.85	112	96	7	203	240	190	192
12	1114:30	43	0.31	1.5	113	96	6	209	242	190	190
B1	1137		0.48	2.35	98	94	8	152	167	170	200
2	1139:30	1142	0.45	2.4	99	92	8	162	208	185	204
3	1142		0.52	2.58	98	90	7	179	210	220	206
4	1224:30		0.51	2.75	99	92	7	190	240	200	210
5	1227		0.53	2.59	99	93	8	210	260	210	211
6	1229:30		0.52	2.58	100	95	8	230	280	215	212
7	1232		0.52	2.58	108	95	9	247	290	195	212
8	1234:30		0.53	2.59	110	96	9	247	290	195	209
9	1237		0.50	2.45	112	98	9	247	290	195	208
10	1239:30		0.43	2.10	115	96	8	245	290	195	199
11	1242		0.34	1.66	115	96	6	244	290	195	197
12	1244:30		0.29	1.42	115	96	6	242	288	195	192
	1247	520									
*	0	42.368		delta H =	T _m =						T _s =

* Sum, average or Difference

Pre-Leak Check 0.009 @ 15Post Leak Check ✓FYRITE: % OXYGEN 20.5
% CARBON DIOXIDE 0.0

CLIENT: JAMES H. MOORE
 SAMPLING DATE: 2/1/89
 SAMPLING TIME: 1047-1247
 UNIT SAMPLED: INLET

Date: 02/26/89
 Time: 10:54 AM
 Run # 3

AVERAGE VELOCITY PRESSURE

Delta P (IN H2O)	Delta P SQUARE ROOT
0.45	0.70
0.47	0.69
0.56	0.75
0.57	0.77
0.58	0.76
0.58	0.76
0.55	0.74
0.49	0.70
0.48	0.69
0.56	0.60
0.58	0.62
0.51	0.56
0.48	0.69
0.49	0.70
0.52	0.72
0.57	0.75
0.53	0.73
0.52	0.72
0.52	0.72
0.53	0.73
0.50	0.71
0.43	0.66
0.34	0.58
0.29	0.54

THE AVERAGE SQUARE ROOT OF DELTA P = 0.6710185

CLIENT: MAXWELL HOUSE
 SAMPLING DATE: 2/1/89
 SAMPLING TIME: 1047-1247
 UNIT SAMPLED: INLET

Date: 02/25/89
 Time: 10:34 AM
 Run # 3

Delta H (IN H2O)	Meter Temp(F) IN	Stack Temp(F) OUT
2.40	98.00	88.00
2.30	90.00	88.00
2.70	94.00	88.00
2.90	99.00	90.00
2.80	102.00	90.00
2.80	104.00	92.00
2.70	100.00	92.00
2.40	108.00	92.00
2.30	106.00	92.00
1.70	111.00	94.00
1.60	112.00	96.00
1.50	113.00	96.00
2.30	98.00	94.00
2.40	99.00	92.00
2.08	98.00	90.00
2.79	99.00	92.00
2.09	99.00	93.00
2.08	100.00	93.00
2.08	108.00	95.00
2.09	110.00	96.00
2.40	112.00	98.00
2.10	113.00	96.00
1.60	113.00	96.00
1.42	113.00	96.00
		195.00
		197.00
		198.00
		199.00
		200.00
		201.00
		202.00
		201.00
		197.00
		194.00
		192.00
		190.00
		200.00
		204.00
		206.00
		210.00
		211.00
		212.00
		212.00
		209.00
		205.00
		199.00
		197.00
		192.00

AVERAGES

DELTA H = 2.36 IN H2O
 METER TEMP. = 98.5625 F
 STACK TEMP. = 201.0417 F

SAMPLE LOCATION INLETRUN NO. 3DATE 2/1/89

CHAIN-OF-CUSTODY SAMPLE NO. _____

	GRAMS
IMPINGER 1	FINAL WEIGHT <u>763.1</u> INITIAL WEIGHT <u>720.1</u> INCREASE
IMPINGER 2	FINAL WEIGHT <u>737.1</u> INITIAL WEIGHT <u>708.4</u> INCREASE
IMPINGER 3	FINAL WEIGHT <u>482.0</u> INITIAL WEIGHT <u>479.7</u> INCREASE
SILICA GEL	FINAL WEIGHT <u>776.0</u> INITIAL WEIGHT <u>761.2</u> INCREASE

	GRAMS
IMPINGER 1	<u>42.4</u>
IMPINGER 2	<u>28.5</u>
IMPINGER 3	<u>2.3</u>
SILICA GEL	<u>88.0</u>

TOTAL MASS OF WATER CAUGHT

GRAMS

CHAIN-OF-CUSTODY SAMPLE NO. _____

FILTER DIAMETER 4 INCHESFILTER TYPE Glass Fiber

FILTER:	FINAL WEIGHT <u>.6716</u> GMS
	INITIAL WEIGHT <u>.6203</u> GMS
	INCREASE

<u>.0511</u>	GRAMS
--------------	-------

TOTAL MASS OF PARTICULATE CAUGHT THIS FILTER

IS ICE PRESENT IN THE IMPINGER BATH AT THE END OF THIS SAMPLE? YES _____ NO _____

CALCULATIONS

$$V_{m-std} = 17.65 (V_m) \left(\frac{P_{bar} + \Delta H / 13.6}{T_m + 460} \right) = 17.65 () \left(\frac{+ 13.6}{+ 460} \right)$$

$$= 17.65 () () = \text{_____} \text{ FT}^3$$

$$V_{m-std} (H_2O) = \frac{\text{GRAMS COLLECTED}}{21.2 \text{ GRAMS/FT}^3} = \frac{()}{(21.2)} = \text{_____} \text{ FT}^3$$

$$X_{H_2O} = \frac{(V_{m-std}) 100}{((V_{m-std}) + (V_{m-std}))} = \frac{100 ()}{() + ()} = \frac{()}{()} = \text{_____} \%$$

$$\text{MOLECULAR WEIGHT (MW)} = \frac{18 (X_{H_2O})}{100} + \frac{\text{DRY MW} (100 - X_{H_2O})}{100} = 0.18 () + \frac{() ()}{100}$$

$$\text{VELOCITY (ACTUAL) IN STACK} = 85.48 (Cp) \sqrt{\frac{T_s + 460}{P_s (MW)}} \sqrt{\Delta P} = 85.48 () \sqrt{\frac{()}{() ()}} \sqrt{\Delta P}$$

$$V_s = () \sqrt{\Delta P} = () () \sqrt{\Delta P}$$

$$V_s = () \Delta P = () () = \text{_____} \text{ FT/SEC}$$

$$\text{ACFM} = (V_s) (60) (CSA) = () (60) () = \text{_____}$$

$$\text{VELOCITY @ Std } V_{s-std} = V_s (17.65) \left(\frac{P_s}{T_s + 460} \right) = () (17.65) () = \text{_____} \text{ FT/SEC}$$

$$\text{SCFM} = (V_{s-std}) (CSA) (60) = () () (60) = \text{_____}$$

$$\text{DSCFM} = \left(\frac{100 - X_{H_2O}}{100} \right) (\text{SCFM}) = () () = \text{_____}$$

$$\text{NOZZLE VELOCITY @ STD } V_n = \frac{(V_{m-std} + V_{m-std})}{60 (8) A_n} = \frac{()}{60 () () (10^{-4})} = \text{_____} \text{ FT/SEC}$$

$$I = \frac{100 V_{n-std}}{V_{s-std}} = \frac{100 ()}{()} = \text{_____} \% \text{ Isokinetic}$$

LAB DATA - EVAPORATIONS

0 030

PLANT MANWELL House

SAMPLE LOCATION Inlet

RUN NO. 3 FOR

SAMPLING DATE 2-1-89

OPERATING CONDITION

CHAIN-OF-CUSTODY SAMPLE NO.

ACETONE WASHINGS

GROSS 655.7 GMS
 TOTAL TARE - 460.2 GMS
 SAMPLE (A) NET 195.5 GMS
 AMOUNT EVAPORATED (B) 195.5 GMS
 EVAP. BEAKER NO. _____
 GROSS 96.7241 GMS
 TARE - 96.6887 GMS
 (C) NET 0.0354 GMS

ACETONE BLANK

EVAP. BEAKER NO. _____
99.6314 GROSS 96.7241 GMS
99.6316 TARE - 96.6887 GMS
 D NET 0.0354 GMS
 ACETONE BLANK = NET 100 GMS (D)
 TOTAL AMOUNT EVAPORATED 100 GMS (F)

$$\text{CORRECTED NET (E)} = (C) - (B) \left[\frac{(D)}{(F)} \right]$$

$$= 0.0354 - 195.5 \left[\frac{100}{100} \right]$$

$$= 0.0354 \text{ GMS (E) } = (C) - B \left[\frac{(D)}{(F)} \right]$$

$$\text{SCALED UP NET} = (E) \left(\frac{A}{B} \right)$$

$$= 0.0354 \left(\frac{195.5}{195.5} \right)$$

$$= 0.0354 \text{ GMS}$$

WET CATCH

GROSS _____ GMS
 TOTAL TARE - _____ GMS
 SAMPLE (A) NET _____ GMS
 AMOUNT EXTRACTED (B) _____ GMS (MLS)
 AMOUNT OF E/C _____ GMS (H)

WATER PHASE
 EVAP. BEAKER NO. _____
 GROSS _____ GMS
 TARE - _____ GMS
 (J) NET _____ GMS
 WATER BLANK
 (L) = _____ GMS
100 GMS

$$\text{CORRECTED NET (N)} = J - (G)(L)$$

$$= \text{_____} \left(\frac{100}{100} \right)$$

$$= \text{_____} \text{ GMS}$$

$$\text{SCALED UP NET} = (N) \left(\frac{E}{A} \right)$$

$$= \text{_____} \left(\frac{0.0354}{195.5} \right)$$

$$= \text{_____} \text{ GMS}$$

EC PHASE
 EVAP. BEAKER NO. _____
 GROSS _____ GMS
 TARE - _____ GMS
 (K) NET _____ GMS
 E/C BLANK
 (M) = _____ GMS
100 MLS

$$\text{CORRECTED NET (N)} = K - (H)(M)$$

$$= \text{_____} \left(\frac{100}{100} \right)$$

$$= \text{_____} \text{ GMS}$$

$$\text{SCALED UP NET} = (P) \left(\frac{E}{G} \right)$$

$$= \text{_____} \left(\frac{0.0354}{195.5} \right)$$

$$= \text{_____} \text{ GMS}$$

UNITED STATES

DEPARTMENT OF COMMERCE, BUREAU OF STANDARDS, WASHINGTON, D. C. 20536

STANDARD GRADE

UNITED STATES OF AMERICA

ORGANIC PHASE

ORGANIC PHASE

UNITED STATES OF AMERICA
DEPARTMENT OF COMMERCE
BUREAU OF STANDARDS
WASHINGTON, D. C. 20536

STANDARD GRADE

UNITED STATES OF AMERICA

DEPARTMENT OF COMMERCE

BUREAU OF STANDARDS

WASHINGTON, D. C. 20536

STANDARD GRADE

UNITED STATES OF AMERICA

DEPARTMENT OF COMMERCE

BUREAU OF STANDARDS

WASHINGTON, D. C. 20536

STANDARD GRADE

UNITED STATES OF AMERICA

DEPARTMENT OF COMMERCE

BUREAU OF STANDARDS

WASHINGTON, D. C. 20536

STANDARD GRADE

UNITED STATES OF AMERICA

DEPARTMENT OF COMMERCE

BUREAU OF STANDARDS

WASHINGTON, D. C. 20536

STANDARD GRADE

UNITED STATES OF AMERICA

DEPARTMENT OF COMMERCE

BUREAU OF STANDARDS

WASHINGTON, D. C. 20536

STANDARD GRADE

UNITED STATES OF AMERICA

INLET

0 072

CLIENT: LAWRENCE HUBER

Date: 02-16/87

Time: 10:14 AM

THE FOLLOWING WERE PROGRAMMER INPUTS FOR ISORINETICS

PARAMETER	1	2	3
DATE	12/31/87	12/31/87	12/31/87
TIME	1000-1140	0600-0720	1047-1247
Unit: SAMPLES	INLET	INLET	INLET
ACTUAL NOZZLE DIAMETER (IND), IN	0.25	0.25	0.25
FITTED FACTOR (CF)	0.99	0.99	0.99
TIME BETWEEN POINTS (MIN)	2.00	2.50	2.50
AMBIENT PRESSURE (BAR), IN-HG	29.77	29.78	29.80
STACK PRESSURE (PSI), IN-HG	-4.50	-4.50	-4.20
NO FLOW VOLUME AVG, GPM	44.74	47.00	44.28
WATER COLLECTED INTERVAL, GPM	74.50	73.50	68.00
CARBON DIOXIDE (CO ₂), %	0.00	0.00	0.00
OXYGEN (O ₂), %	20.00	21.00	21.00
STACK DIAMETER (DIA), IN	11.50	11.50	11.50
STACK CROSS SECTIONAL AREA (SQ IN)	0.72	0.72	0.72

CALCULATION OF ISUKINETIC

Date: 10/10/67

Time: 10:24 AM

ISUKINETIC CALCULATIONS

Parameter	1	2	3
Date	12/17/67	2/17/67	2/17/67
Case	1000-1145	0802-0921	1000-1145
Unit Sampled	INLET	INLET	IN
METER VOLUME (VM-STD), SCU-FT	41.08	44.59	41.95
WATER COLLECTED (WM-STD), SCU-FT	4.49	4.43	4.17
MOISTURE (VOL %)	7.83	9.04	9.03
ACTUAL MOLECULAR WEIGHT (MW), LBS/LB-MOLE	27.83	27.86	27.86
ACTUAL VELOCITY IN STACK (VS), FT/SEC	42.42	33.23	32.41
ACTUAL FLOW RATE IN STACK (ACFM)	2137.98	2303.55	2267.38
VELOCITY @ STP (VS-STD), FT/SEC	41.58	42.47	41.41
STACK FLOW RATE @ STP (SCFM)	1796.54	1837.91	1791.54
DRY FLOW RATE (DSCFM)	1621.45	1671.82	1629.72
NOZZLE VELOCITY @ STP (VN-STD), FT/SEC	37.13	39.95	37.58
ISUKINETIC %	89.32	94.03	90.73

0 074

PARTICULATE FIELD

DATA BOOK

DAILY
STACK/AIR
TESTING
FIELD REPORT

F-19 (7.13.88)

cc: billing _____
chron _____
Original to Job file _____

Date 1-31-89 Client _____

RECON Job No. _____
Project Manager _____
Field Supervisor _____

Jobsite Company _____ Street _____

City _____ State _____ Zip _____ Phone _____

Processes, Stacks, Vents, Air etc. Tested Today

1. Afterburner Outlet Condition* _____
2. _____ Condition* _____
3. _____ Condition* _____
4. _____ Condition* _____

* (e.g. stack opacity, raining?, odors, color, flowrate; process steady or upset; etc.)

Milestone Times (Military)

Departure from home or RECON _____ Arrival at site _____ Lunch _____ to _____

Lost Time _____ to _____ Arrival at home or RECON _____

Reason For Lost Time _____

Client or Job Site Rep Aware of Lost Time _____ yes _____ no _____ Person _____

Personnel Onsite

RECON _____

Client _____

Jobsite Reps _____

Agency Observing (1) ATOSP (2) _____Agency Personnel MIKE CIOSEK _____

Other _____

Out of Scope Work Requested and Performed

PARTICULATE.ATG (August 1988)

AirRecon
THREE BRIDGES, NJ

PRELIMINARY DATA

COMPANY:

GENERAL FOODS

SAMPLE LOCATION:

OUTLET

0 075

DATE:

1/30/89

TIME:

PITOT TUBE LINES LEAK CHECK



LEVEL AND ZERO MANOMETER



ESTIMATED MOISTURE -(%)

C_p

DRY BULB -(°F)

WET BULB -(°F)

DIRECTION OF FLOW

TRAVERSE POINT NUMBER	CYCLONIC FLOW ANGLE THAT YIELDS A NULL DELTA P	VELOCITY HEAD DELTA P INCHES OF H ₂ O	STACK TEMPERATURE (DEGREES F)
A-1	5		
2	3		
3	2		
4	2		
5	2		
6	3		
7	3		
8	7		
9	7		
10	6		
11	4		
12	6		
B-1	8		
2	7		
3	7		
4	4		
5	4		
6	3		
7	4		
8	6		
9	5		
10	6		
11	7		
12	7		
AVERAGE			

AVERAGE ANGLE MUST BE <20 DEGREES

k = 17.0

PARTICULATE FIELD DATA SHEET

0 070

PLANT MAYWELL HOUSE DATE 1-31-89 RUN NO. 1

SAMPLE LOCATION AFTERBURNER OUTLET RAC BOX NO. 4 DRY GAS METER NO. 175176

NOZZLE NO. 6 NOZZLE SIZE 1/2 INCHES PITOT NO. 19 C_p .83

TIME AT EACH POINT (0) 3 MINUTES DELTA H @ 2.00 THERMOCOUPLE NO.: T 41

AMBIENT PRESSURE (P_{BAR}) 29.91 "HG PROBE OUTLET 38

STATIC PRESSURE (P) -0.02 "H₂O/13.6 = _____ "Hg(P meter) BOX OUTLET 18

STACK PRESSURE (P_s) = P_{bar} + P_{meter} = _____ "Hg OPERATING CONDITION OR REMARKS _____

DRY BULB _____ °F WET BULB _____ °F _____ %H₂O

PORT/ POINT	MILITARY CLOCK TIME	METER READING	PITOT DELTA P "H ₂ O	ORIFICE DELTA H "H ₂ O	METER TEMP. °F		LINE VAC "Hg	PROBE OUTLET °F	BOX OUTLET TEMP °F	BOX TEMP °F	STACK TEMP °F
					IN	OUT					
A-1	1000	91.722	.05	.85	77	77	4+	188	195	220	1555
2	03	93.3	.05	.85	78	77	4+	188	196	221	1550
3	06	95.1	.06	1.02	79	77	4+	200	197	223	1520
4	09	96.3	.06	1.02	81	78	4+	201	198	221	1516
5	12	98.4	.07	1.18	83	78	4+	202	200	223	1485
6	15	100.0	.07	1.18	85	78	5+	201	201	220	1530
7	18	101.5	.06	1.02	86	78	5	200	205	228	1535
8	21	102.8	.06	1.02	87	79	5	200	202	227	1538
9	24	104.5	.055	.93	88	79	4+	201	203	228	1494
10	27	106.6	.07	1.18	89	80	5+	201	204	225	1485
11	30	108.0	.07	1.18	90	80	5+	202	203	226	1498
12	33	109.1	.07	1.18	91	81	5+	200	204	225	1498
END	36	110.77									
B-1	1115	110.85	.06	1.02	82	82	5+	188	200	223	1501
2	18	112.5	.06	1.02	83	81	5+	189	201	225	1520
3	21	114.2	.07	1.18	84	80	5+	189	202	226	1502
4	24	116.0	.07	1.18	86	81	5+	198	203	225	1493
5	27	117.5	.07	1.18	89	81	5+	198	204	226	1495
6	30	119.9	.075	1.25	90	81	5+	203	208	228	1501
7	33	121.9	.075	1.25	92	82	5+	204	210	225	1493
8	36	122.4	.075	1.25	92	82	5+	206	211	227	1488
9	39	124.3	.07	1.18	93	83	5+	205	212	226	1497
10	42	126.1	.07	1.18	94	83	5+	208	213	226	1498
11	45	127.7	.07	1.18	94	83	5+	207	214	227	1488
12	48	129.8	.075	1.25	95	83	5+	207	213	225	1482
END	51	131.244	delta H =	T _m =						T _s =

* Sum, average or Difference

Pre-Leak Check 0.01 at 15" Post Leak Check 0.004 at 57" FYRITE: % OXYGEN 14.0

% CARBON DIOXIDE 4.0

PARTICULATE.ATG (August 1988)

NOTE METER REMAINING CHANGE BETWEEN PORTS

AirRecon
THREE BRIDGES, NJ

SUBJECT: RECENTLY

Date: 02/07/87

Time: 10:55 AM

AVERAGE VELOCITY PRESSURE

Delta F (in Hz)	Delta F Square Root
0.02	0.22
0.02	0.22
0.06	0.24
0.06	0.24
0.07	0.26
0.07	0.26
0.06	0.24
0.06	0.24
0.06	0.23
0.07	0.26
0.07	0.26
0.07	0.26
0.06	0.24
0.06	0.24
0.07	0.26
0.07	0.26
0.07	0.26
0.06	0.24
0.06	0.24
0.07	0.26
0.07	0.26
0.07	0.26
0.06	0.24
0.06	0.24
0.07	0.26
0.07	0.26
0.07	0.26
0.06	0.24

THE AVERAGE SQUARE ROOT OF DELTA P = .25650

0 073

CLIENT: MCKELL, ARDIE

Date: 07/07

Time: 10:00 AM

Delta P (IN H2O)	Meter Temp (F)		Stack Temp (F)
	IN	OUT	
0.91	77.00	77.00	1333.00
0.94	78.00	77.00	1330.00
1.00	77.00	77.00	1320.00
1.02	81.00	76.00	1316.00
1.10	83.00	78.00	1485.00
1.18	85.00	78.00	1330.00
1.02	86.00	78.00	1333.00
1.02	87.00	79.00	1338.00
0.93	88.00	79.00	1494.00
1.18	89.00	80.00	1485.00
1.18	90.00	80.00	1498.00
1.18	91.00	81.00	1498.00
1.02	82.00	82.00	1501.00
1.02	83.00	81.00	1520.00
1.18	84.00	80.00	1502.00
1.18	86.00	81.00	1493.00
1.18	89.00	81.00	1495.00
1.25	90.00	81.00	1501.00
1.25	92.00	82.00	1493.00
1.25	92.00	82.00	1488.00
1.18	93.00	83.00	1477.00
1.18	94.00	83.00	1478.00
1.18	94.00	83.00	1478.00
1.25	95.00	83.00	1482.00

AVERAGES

DELTA P = 1.11375 IN H2O

METER TEMP. = 83.5834 F

STACK TEMP. = 1506.333 F

HYDROCARBON SAMPLING DATA

SAMPLE LOCATION Affluence, OntarioRUN NO. 1DATE 1-31-89

HYDROCARBON PUMP NO. _____

TIME	ROTOMETER SETTING	GAS METER TEMP.	VACUUM "HG	SAMPLE RATE L/M
1000	60	82	1+	1
05	60	82	1+	1
10	60	83	1+	1
15	60	83	1+	1
20	60	84	1+	1
25	60	84	1+	1
30	60	85	1+	1
1115	60	86	1+	1
20	60	86	1+	1
35	60	86	1+	1
40	60	87	1+	1
50	60	87	1+	1
		88		

PRE-LEAK CHECK ✓POST-LEAK CHECK ✓

PUMP CALIBRATION FLOW RATE		CALIBRATION INSTRUMENT		FYRITE	
FLOW RATE	ROTAMETER	✓	SOAP FILM BURET		% OXYGEN
LITERS/MIN	SETTING		DRY GAS METER		% CARBON DIOXIDE
1	60		OTHER _____		

CORRECTING ROTOMETER VOLUME TO DRY STANDARD CONDITIONS

$$\text{EQUATION: } V_{STD} = V_M \times \frac{P_M}{T_M} \times \frac{T_{STD}}{P_{STD}}$$

WHERE:

 V_M = SAMPLE RATE OF ROTOMETER (L/M) T_{STD} = $70^{\circ}\text{F} + 460^{\circ}\text{F} = 530^{\circ}\text{F}$ P_{STD} = 29.92"HG P_M = BAROMETRIC PRESSURE DURING SAMPLING ("HG) T_M = TEMPERATURE OF GAS STREAM (+460°F)

$$V_{STD} = \quad \times \left(\frac{\quad}{\quad} \right) \times \frac{(530)}{(29.92)} = \quad$$

$$\text{CF} = (V_{STD} \text{ L/MIN}) (3.53 \times 10^{-2} \text{ CF/L}) (60 \text{ MIN/1 HR}) = (\quad) (3.53 \times 10^{-2}) (60)$$

= CFH

PARTICULATE.ATG (AUGUST 1988)

AirRecon
THREE BRIDGES, NJ

Method #5 Gas and Impinger Contents Data Sheet

Company Name: MAXWELL HOUSE
 Device: AFTERBURNER OUTLET
 Location: HOBOKEN, NJ
 Imp. #1: 1
 Catch Vol. #: _____
 Day Vol. #: _____

Total Wet Catch (mls): 44.00
 Sample Volume (Std. Ft3): 2.12
 Stack Flowrate (DSCFM): 2013.00
 Stack % Moisture: 7.90

Contaminant #	Name	MW	GC: Liquid Concentration (mg/l)	GC: Gas Concentration (ppmv)
(1)	ETHYL AS METHANE	16.05	1.000	19.000
(2)	CARBON MONOXIDE	28.01	0.000	131.000
(3)				
(4)				
(5)				
(6)				
(7)				
(8)				
(9)				
(10)				

Concentrations and Emissions

Contaminant #	Name	LB/HR	PPMV (WET)	PPMV (DRY)
(1)	ETHYL AS METHANE	0.101	18.315	20.103
(2)	CARBON MONOXIDE	1.145	120.651	131.000
(3)		0.000	ERR	ERR
(4)		0.000	ERR	ERR
(5)		0.000	ERR	ERR
(6)		0.000	ERR	ERR
(7)		0.000	ERR	ERR
(8)		0.000	ERR	ERR
(9)		0.000	ERR	ERR
(10)		0.000	ERR	ERR

This Program Uses the Following Equations for Each Contaminant Where:

A = Total Wet Catch (mls)
 B = Sample Volume (Std. Ft3)
 C = Stack Moisture (%)
 D = Stack Flowrate (DSCFM)

E = GC: Liquid Concentration (mg/l)
 F = GC: Gas Concentration (dry ppmv)
 G = Contaminant's Molecular Weight

for the Impinger Contents:

$$\begin{aligned} \text{Wt1} &= \text{dry ppmv} = (0.85313 \times (A) \times (E)) / ((B) \times (D)) \\ \text{Wt2} &= \text{wet ppmv} = (\text{dry ppmv}) \times (100 - (C)) / 100 \\ \text{Wt3} &= \text{pounds/hr} = 0.00000015226 \times (A) \times (E) \times (D) / (B) \end{aligned}$$

for the Gas Bag Contents:

$$\begin{aligned} \text{Wt1} &= \text{dry ppmv} = \text{Wt2} \\ \text{Wt2} &= \text{wet ppmv} = (\text{dry ppmv}) \times (100 - (C)) / 100 \\ \text{Wt3} &= \text{pounds/hr} = 0.00000015205 \times (\text{dry ppmv}) \times (D) \times (G) \end{aligned}$$

AGGREGATE EMISSIONS:

$$\begin{aligned} \text{Wt ppmv} &= (\text{Wt1}) + (\text{Wt2}) \\ \text{Ct ppmv} &= (\text{Wt1}) + (\text{Wt2}) \\ \text{Wt3 lb/hr} &= (\text{Wt3}) + (\text{Wt3}) \end{aligned}$$

MOISTURE DETERMINATION

SAMPLE LOCATION Afterburner OutletRUN NO. 1DATE 1-31-89

CHAIN-OF-CUSTODY SAMPLE NO. _____

		GRAMS
IMPINGER 1	FINAL WEIGHT	<u>757.3</u>
	INITIAL WEIGHT	<u>724.6</u>
	INCREASE	
IMPINGER 2	FINAL WEIGHT	<u>728.4</u>
	INITIAL WEIGHT	<u>712.9</u>
	INCREASE	
IMPINGER 3	FINAL WEIGHT	<u>480.5</u>
	INITIAL WEIGHT	<u>475.2</u>
	INCREASE	
SILICA GEL	FINAL WEIGHT	<u>855.1</u>
	INITIAL WEIGHT	<u>838.9</u>
	INCREASE	

TOTAL MASS OF WATER CAUGHT

GRAMS

IMPINGER 1	<u>32.7</u>
IMPINGER 2	<u>15.5</u>
IMPINGER 3	<u>4.9</u>
SILICA GEL	<u>69.3</u>

GRAMS

CHAIN-OF-CUSTODY SAMPLE NO. _____

FILTER DIAMETER 4 INCHESFILTER TYPE Glass fiber

FILTER:	FINAL WEIGHT	<u>.6475</u>	GMS
	INITIAL WEIGHT	<u>.6278</u>	GMS
	INCREASE		

<u>0.0197</u>	GRAMS
---------------	-------

TOTAL MASS OF PARTICULATE CAUGHT THIS FILTER

IS ICE PRESENT IN THE IMPINGER BATH AT THE END OF THIS SAMPLE? YES _____ NO _____

CALCULATIONS

$$V_{m-std} = 17.65 (V_m) \left(\frac{P_{bar} + \Delta H / 13.6}{T_m + 460} \right) = 17.65 () \left(\frac{ + 13.6 }{ } \right)$$

$$= 17.65 () () = \text{_____} \text{ FT}^3$$

$$V_{w-std} (H_2O) = \frac{\text{GRAMS COLLECTED}}{21.2 \text{ GRAMS/FT}^3} = \frac{()}{(21.2)} = \text{_____} \text{ FT}^3$$

$$\% H_2O = \frac{(V_{w-std}) 100}{((V_{m-std}) + (V_{w-std}))} = \frac{100 ()}{() ()} = \frac{()}{()} = \text{_____} \%$$

$$\text{MOLECULAR WEIGHT (MW)} = \frac{18 (\% H_2O)}{100} + \text{DRY MW} \left(\frac{100 - \% H_2O}{100} \right) = 0.18 () + \frac{() ()}{100}$$

$$\text{VELOCITY (ACTUAL) IN STACK} = 85.48 (C_p) \sqrt{\frac{T_s + 460}{P_s (MW)}} \sqrt{\Delta P} = 85.48 () \sqrt{\frac{()}{() ()}} \sqrt{\Delta P}$$

$$V_s = () \sqrt{\Delta P} = () () \sqrt{\Delta P}$$

$$V_s = () \Delta P = () () = \text{_____} \text{ FT/SEC}$$

$$ACFM = (V_s)(60)(CSA) = () (60) () = \text{_____}$$

$$\text{VELOCITY @ Stp } V_{s-std} = V_s (17.65) \left(\frac{P_s}{T_s + 460} \right) = \frac{() (17.65) ()}{()} = \text{_____} \text{ FT/SEC}$$

$$SCFM = (V_{s-std})(CSA)(60) = () () (60) = \text{_____}$$

$$DSCFM = \left(\frac{100 - \% H_2O}{100} \right) (SCFM) = () () = \text{_____}$$

$$\text{NOZZLE VELOCITY @ STD } V_n = \frac{(V_{m-std} + V_{w-std})}{60 (8) A_n} = \frac{()}{60 () () (10^{-4})} = \text{_____} \text{ FT/SEC}$$

$$I = \frac{100 V_{n-std}}{V_{s-std}} = \frac{100 ()}{()} = \text{_____} \% \text{ Isokinetic}$$

LAB DATA - EVAPORATIONS

PLANT MAXWELL HOUSE

SAMPLE LOCATION Inlet

RUN NO. 1 FOR 0 03

SAMPLING DATE 1/31/89

OPERATING CONDITION _____

CHAIN-OF-CUSTODY SAMPLE NO. _____

ACETONE WASHINGS

GROSS 653.6 GMS
TOTAL SAMPLE TARE - 455.9 GMS
(A) NET 197.7 GMS
AMOUNT EVAPORATED (B) 197.7 GMS
EVAP. BEAKER NO. _____
GROSS 99.8895 GMS
TARE - 99.8811 GMS
(C) NET 0.0084 GMS

ACETONE BLANK

EVAP. BEAKER NO. _____
99.6314 GROSS 99.8895 GMS
99.6316 TARE - 99.8811 GMS
0 NET _____ GMS

ACETONE BLANK = NET 100 GMS (D)
TOTAL AMOUNT EVAPORATED 100 GMS (F)

CORRECTED NET (E) = (C) - (B) $\left[\frac{(D)}{(F)} \right]$
= 0.0084 - 197.7 $\left[\frac{100}{100} \right]$
= 0.0084 GMS (E) = (C) - B $\left[\frac{(D)}{(F)} \right]$

SCALED UP NET = (E) $\left(\frac{A}{B} \right)$
= 0.0084 $\left(\frac{197.7}{197.7} \right)$
= 0.0084 GMS

WET CATCH

GROSS _____ GMS
TOTAL SAMPLE TARE - _____ GMS
(A) NET _____ GMS
AMOUNT EXTRACTED (G) _____ GMS (MLS)
AMOUNT OF E/C _____ GMS (H)

WATER PHASE EVAP. BEAKER NO. _____
GROSS _____ GMS
TARE - _____ GMS
(J) NET _____ GMS
WATER BLANK (L) = 100 GMS

CORRECTED NET (N) = J - (G)(L)
= _____ $\left(\frac{100}{100} \right)$
= _____ GMS
SCALED UP NET = (N) $\left(\frac{E}{G} \right)$
= _____ $\left(\frac{100}{100} \right)$
= _____ GMS

EC PHASE EVAP. BEAKER NO. _____
GROSS _____ GMS
TARE - _____ GMS
(K) NET _____ GMS
E/C BLANK (M) = 100 MLS

CORRECTED NET (P) = K - (N)(M)
= _____ $\left(\frac{100}{100} \right)$
= _____ GMS
SCALED UP NET = (P) $\left(\frac{E}{G} \right)$
= _____ $\left(\frac{100}{100} \right)$
= _____ GMS

Net Weight and Acetone Washing 0.0084 grms

Net Weight 0.0084 grms

By Organic or Aqueous Phase

Aqueous Phase 0 grms

Organic Phase 0 grms

Totals

GRAINS/DSCF = 1.128415E-02
 POUNDS/HOUR = .1946989

HIT RETURN TO CONTINUE

0 034

PARTICULATE FIELD DATA SHEET

PLANT Maxwell HouseDATE 2-1-89RUN NO. 2SAMPLE LOCATION Aftersburn OutletRAC BOX NO. 4DRY GAS METER NO. 175176NOZZLE NO. NOZZLE SIZE 1/2 INCHESPITOT NO. 19C_p .83TIME AT EACH POINT (05 2 1/2) MINUTESDELTA H₂ 2.00THERMOCOUPLE NO.: 41AMBIENT PRESSURE (P_{BAR}) 29.78 "HGPROBE OUTLET 38BOX OUTLET 18STATIC PRESSURE (P) -0.02 "H₂O/13.6 = "Hg(P meter)STACK PRESSURE (P_s) = P_{bar} + P_{meter} = "Hg OPERATING CONDITION OR REMARKS DRY BULB °F WET BULB °F "H₂O

PORT/ POINT	MILITARY CLOCK TIME	METER READING	PITOT DELTA P "H ₂ O	ORIFICE DELTA H "H ₂ O	METER TEMP. °F		LINE VAC "Hg	PROBE OUTLET °F	BOX OUTLET TEMP °F	BOX TEMP °F	STACK TEMP °F
					IN	OUT					
A-1	0750	151.79	.08	1.48	91	91	2	188	200	223	1523
2	52 1/2	153.2	.08	1.48	92	90	2	189	201	220	1540
3	55	154.9	.085	1.70	92	90	2	191	205	226	1545
4	57 1/2	156.4	.07	1.30	94	91	2	194	204	228	1544
5	0800	157.4	.07	1.30	94	91	2	197	206	227	1528
6	02 1/2	159.5	.07	1.30	96	91	2	198	207	228	1499
7	5	161.4	.07	1.30	99	92	2	200	204	225	1530
8	07 1/2	163.1	.065	1.20	99	92	H	201	208	222	1524
9	10	164.3	.065	1.20	100	92	H	201	208	226	1535
10	12 1/2	165.3	.065	1.20	100	92	H	202	209	228	1534
11	15	167.0	.06	1.10	100	92	H	203	210	227	1503
12	17 1/2	168.2	.055	1.02	100	92	H	204	212	224	1488
END	0820	169.76									
B-1	0850	169.78	.05	.93	89	89	H	195	198	219	1484
2	02 1/2	171.5	.08	1.50	88	89	2	198	199	220	1520
3	55	172.3	.08	1.50	88	87	2	198	200	223	1530
4	57 1/2	174.5	.07	1.30	90	87	2	199	201	228	1530
5	0900	175.5	.07	1.30	91	87	2	200	203	229	1500
6	02 1/2	177.5	.075	1.40	94	87	2	201	204	227	1495
7	05	178.8	.075	1.40	95	88	2	201	203	225	1493
8	07 1/2	180.4	.07	1.30	96	88	2	202	203	226	1496
9	10	181.9	.06	1.10	97	88	2	203	203	225	1493
10	12 1/2	183.0	.06	1.10	97	88	2	204	203	226	1495
11	15	184.0	.05	.92	98	88	2	204	204	224	1490
12	17 1/2	184.9	.05	.93	99	88	2	204	204	225	1498
END	0920	187.04	delta H =	T _m =						T _s =

* Sum, average or Difference

Pre-Leak Check 0.00 at 15"Post Leak Check 0.00 at 3"

FYRITE:

% OXYGEN 15.0% CARBON DIOXIDE 6.0

PARTICULATE.ATG (August 1988)

NOTE METER READING CHANGE BETWEEN PORTS.

AirRecon
THREE BRIDGES, NJ

CLIENT: CARROLL HOUSE

Date: 02/26/89

Time: 10:38 AM

AVERAGE VELOCITY PRESSURE

Delta P	Delta P
(in H ₂ O)	Square Root
0.07	0.26
0.06	0.25
0.07	0.27
0.07	0.26
0.07	0.26
0.07	0.26
0.07	0.26
0.07	0.26
0.07	0.26
0.06	0.24
0.06	0.23
0.05	0.22
0.08	0.28
0.08	0.28
0.07	0.26
0.07	0.26
0.08	0.27
0.08	0.27
0.07	0.26
0.06	0.24
0.06	0.24
0.05	0.22
0.05	0.22

THE AVERAGE SQUARE ROOT OF DELTA P = 0.2594878

CLIENT: BOWWELL HOUSE

Date: 02/26/89

Time: 10:38 AM

Delta H (IN H2O)	Meter Temp (F)		Stack Temp (F)
	IN	OUT	
1.46	91.00	91.00	1523.00
1.46	92.00	90.00	1540.00
1.70	92.00	90.00	1545.00
1.30	94.00	91.00	1544.00
1.30	94.00	91.00	1528.00
1.30	96.00	91.00	1499.00
1.30	99.00	92.00	1530.00
1.20	99.00	92.00	1524.00
1.20	100.00	92.00	1535.00
1.20	100.00	92.00	1534.00
1.10	100.00	92.00	1503.00
1.02	100.00	92.00	1488.00
0.93	89.00	89.00	1484.00
1.00	88.00	89.00	1520.00
1.00	88.00	87.00	1530.00
1.30	90.00	87.00	1530.00
1.30	91.00	87.00	1500.00
1.40	94.00	87.00	1495.00
1.40	95.00	88.00	1493.00
1.30	96.00	88.00	1496.00
1.10	97.00	88.00	1493.00
1.10	97.00	88.00	1495.00
0.93	98.00	88.00	1490.00
0.93	99.00	88.00	1498.00

AVERAGES

DELTA H = 1.26125 IN H2O

METER TEMP. = 92.27084 F

STACK TEMP. = 1513.208 F

HYDROCARBON SAMPLING DATA

SAMPLE LOCATION OutletRUN NO. 2DATE 2-1-89

HYDROCARBON PUMP NO. _____

TIME	ROTOMETER SETTING	GAS METER TEMP.	VACUUM "HG	SAMPLE RATE L/M
0750	60	74	1+	1
55	60	74	1+	1
0800	60	74	1+	1
05	60	75	1+	1
10	60	75	1+	1
15	60	76	1+	1
20	60	76	1+	1
25	60	76	1+	1
30	60	76	1+	1
35	60	76	1+	1
40	60	76	1+	1
45	60	77	1+	1
0850	60	78	1+	1

PRE-LEAK CHECK ✓POST-LEAK CHECK ✓

PUMP CALIBRATION FLOW RATE		CALIBRATION INSTRUMENT		FYRITE	
FLOW RATE	ROTAMETER	_____	SOAP FILM BURET	_____	% OXYGEN
LITERS/MIN	SETTING	_____	DRY GAS METER	_____	% CARBON DIOXIDE
1	60	_____	OTHER _____	_____	

CORRECTING ROTOMETER VOLUME TO DRY STANDARD CONDITIONS

$$\text{EQUATION: } V_{\text{STD}} = V_{\text{M}} \times \frac{P_{\text{M}}}{T_{\text{M}}} \times \frac{T_{\text{STD}}}{P_{\text{STD}}}$$

WHERE:

 V_{M} = SAMPLE RATE OF ROTOMETER (L/M) T_{STD} = $70^{\circ}\text{F} + 460^{\circ}\text{F} = 530^{\circ}\text{F}$ P_{STD} = 29.92" HG P_{M} = BAROMETRIC PRESSURE DURING SAMPLING ("HG) T_{M} = TEMPERATURE OF GAS STREAM (+460°F)

$$V_{\text{STD}} = \left(\frac{\text{_____}}{\text{_____}} \right) \times \frac{(530)}{(29.92)} = \text{_____}$$

$$\text{CF} = (V_{\text{STD}} \text{ L/MIN}) (3.53 \times 10^{-2} \text{ CF/L}) (60 \text{ MIN/1 HR}) = (\text{_____}) (3.53 \times 10^{-2}) (60)$$

= _____ CFH

Imp. Method #3 Gas and Impinger Contents Data Sheet

Company Name: MAXWELL HOUSE Total Wet Catch (mls): 44.00
 Unit: AFTERBURNER OUTLET Sample Volume (std. Ft3): 2.12
 Location: HUBOKEN, NJ Stack Flowrate (DSCFM): 2035.00
 Run #: 2 Stack % Moisture: 7.60
 Catch I.D.#: _____
 Bag I.D.#: _____

Contaminants	Name	MW	Concentration	
			GC: Liquid (mg/l)	GC: Gas (ppmv)
(1)	THC as METHANE	16.04	0.500	35.000
(2)	CARBON MONOXIDE	28.01	0.000	416.000
(3)				
(4)				
(5)				
(6)				
(7)				
(8)				
(9)				
(10)				

Concentrations		and Emissions		
Contaminants	Name	LB/HR	PPMV (WET)	PPMV (DRY)
(1)	THC as METHANE	0.181	32.952	35.662
(2)	CARBON MONOXIDE	3.677	384.384	416.000
(3)		0.000	ERR	ERR
(4)		0.000	ERR	ERR
(5)		0.000	ERR	ERR
(6)		0.000	ERR	ERR
(7)		0.000	ERR	ERR
(8)		0.000	ERR	ERR
(9)		0.000	ERR	ERR
(10)		0.000	ERR	ERR

This Program Uses the Following Equations for Each Contaminant Where:

W = Total Wet Catch (mls) E = GC: Liquid Concentration (mg/l)
 V = Sample Volume (std. Ft3) F = GC: Gas Concentration (dry ppmv)
 M = Stack Moisture (%) b = Contaminant's Molecular Weight
 Q = Stack Flowrate (DSCFM)

For the Impinger Contents:

$$\begin{aligned} \text{dry ppmv} &= (0.8013 \times (W) \times (E)) / (V \times (b)) \\ \text{wet ppmv} &= (\text{dry ppmv}) \times (100 - (M)) / 100 \\ \text{pounds/hr} &= 0.0000000222 \times (Q) \times (E) \times (b) \end{aligned}$$

For the Gas Gas Concentrations:

$$\begin{aligned} \text{dry ppmv} &= (W) \\ \text{wet ppmv} &= (\text{dry ppmv}) \times (100 - (M)) / 100 \\ \text{pounds/hr} &= 0.0000000222 \times (Q) \times (F) \times (b) \end{aligned}$$

Concentrations and Emissions:

$$\begin{aligned} \text{total dry ppmv} &= (H1) + (H2) \\ \text{total wet ppmv} &= (J1) + (J2) \end{aligned}$$

MOISTURE DETERMINATION

0 080

SAMPLE LOCATION Outlet

RUN NO. 2

DATE 2/1/89

CHAIN-OF-CUSTODY SAMPLE NO. _____

		GRAMS
IMPINGER 1	FINAL WEIGHT	<u>720.9</u>
	INITIAL WEIGHT	<u>696.4</u>
	INCREASE	
IMPINGER 2	FINAL WEIGHT	<u>693.0</u>
	INITIAL WEIGHT	<u>678.2</u>
	INCREASE	
IMPINGER 3	FINAL WEIGHT	<u>499.4</u>
	INITIAL WEIGHT	<u>495.5</u>
	INCREASE	
SILICA GEL	FINAL WEIGHT	<u>720.0</u>
	INITIAL WEIGHT	<u>704.5</u>
	INCREASE	

	GRAMS
IMPINGER 1	<u>24.5</u>
IMPINGER 2	<u>14.8</u>
IMPINGER 3	<u>2.9</u>
SILICA GEL	<u>15.5</u>

TOTAL MASS OF WATER CAUGHT

58.7

GRAMS

CHAIN-OF-CUSTODY SAMPLE NO. _____

FILTER DIAMETER 4 INCHES

FILTER TYPE 6105 filter

FILTER:	FINAL WEIGHT	<u>6514</u>	GMS
	INITIAL WEIGHT	<u>6280</u>	GMS
	INCREASE		

0.0234

GRAMS

TOTAL MASS OF PARTICULATE CAUGHT THIS FILTER

IS ICE PRESENT IN THE IMPINGER BATH AT THE END OF THIS SAMPLE? YES _____ NO _____

CALCULATIONS

$$V_{m-std} = 17.65 (V_m) \left(\frac{P_{bar} + \Delta T / 13.6}{T_m + 460} \right) = 17.65 () \left(\frac{ + 13.6 }{ } \right)$$

$$= 17.65 () () = \text{FT}^3$$

$$V_{w-std} (H_2O) = \frac{\text{GRAMS COLLECTED}}{21.2 \text{ GRAMS/FT}^3} = \frac{ () }{ (21.2) } = \text{FT}^3$$

$$\% H_2O = \frac{(V_{w-std}) 100}{((V_{m-std}) + (V_{w-std}))} = \frac{100 ()}{() ()} = \frac{ () }{ () } = \text{X}$$

$$\text{MOLECULAR WEIGHT (MW)} = \frac{18 (\% H_2O)}{100} + \frac{\text{DRY MW} (100 - \% H_2O)}{100} = 0.18 () + \frac{ () () }{100}$$

$$\text{VELOCITY (ACTUAL) IN STACK} = 85.48 (Cp) \sqrt{\frac{I_s + 460}{P_s (MW)}} \sqrt{\Delta T P} = 85.48 () \sqrt{\frac{ () }{ () () }} \sqrt{\Delta T P}$$

$$V_s = () \sqrt{\Delta T P} = () () \sqrt{\Delta T P}$$

$$V_s = () \Delta T P = () () = \text{FT/SEC}$$

$$\text{ACFM} = (V_s)(60)(CSA) = () (60) () =$$

$$\text{VELOCITY @ Stp } V_{s-std} = V_s (17.65) \left(\frac{P_s}{T_s + 460} \right) = \frac{ () (17.65) () }{ () } = \text{FT/SEC}$$

$$\text{SCFM} = (V_{s-std})(CSA)(60) = () () (60) =$$

$$\text{DSCFM} = \left(\frac{100 - \% H_2O}{100} \right) (\text{SCFM}) = () () =$$

$$\text{NOZZLE VELOCITY @ STD } V_n = \frac{(V_{m-std} + V_{w-std})}{60 (\theta) A_n} = \frac{ () }{ 60 () () (10^{-4}) } = \text{FT/SEC}$$

$$I = \frac{100 V_{n-std}}{V_{s-std}} = \frac{100 ()}{()} = \text{X Isokinetic}$$

LAB DATA - EVAPORATIONS

0 000

PLANT MAXWELL HOUSE

SAMPLE LOCATION Outlet

RUN NO. 2 FOR _____

SAMPLING DATE 2/1/89

OPERATING CONDITION _____

CHAIN-OF-CUSTODY SAMPLE NO. _____

ACETONE WASHINGS

GROSS 659.4 GMS
TOTAL SAMPLE TARE - 457.1 GMS
(A) NET 202.3 GMS
AMOUNT EVAPORATED (B) 202.3 GMS
EVAP. BEAKER NO. _____
GROSS 106.9284 GMS
TARE - 106.9169 GMS
(C) NET 0.0117 GMS

ACETONE BLANK

EVAP. BEAKER NO. _____
99.6314 GROSS 106.9286 GMS
99.6316 TARE - 106.9169 GMS
NET 0 GMS
ACETONE BLANK = NET 0 GMS (D)
TOTAL AMOUNT EVAPORATED 100 GMS (F)

CORRECTED NET (E) = (C) - (B) $\left[\frac{(D)}{(F)} \right]$
= 0.0117 - 202.3 $\left[\frac{0}{100} \right]$
= 0.0117 GMS (E) = (C) - B $\left[\frac{(D)}{(F)} \right]$

SCALED UP NET = (E) $\left(\frac{A}{B} \right)$
= 0.0117 $\left(\frac{202.3}{202.3} \right)$
= 0.0117 GMS

WET CATCH

GROSS _____ GMS
TOTAL SAMPLE TARE - _____ GMS
(A) NET _____ GMS
AMOUNT EXTRACTED (G) _____ GMS (MLS)
AMOUNT OF E/C _____ GMS (H)

WATER PHASE
EVAP. BEAKER NO. _____
GROSS _____ GMS
TARE - _____ GMS
(J) NET _____ GMS
WATER BLANK
(L) = 100 GMS

CORRECTED NET
(N) = J - (G) $\left(\frac{L}{100} \right)$
= _____ $\left(\frac{100}{100} \right)$
= _____ GMS
SCALED UP NET = (N) $\left(\frac{E}{G} \right)$
= _____ $\left(\frac{100}{100} \right)$
= _____ GMS

EC PHASE
EVAP. BEAKER NO. _____
GROSS _____ GMS
TARE - _____ GMS
(K) NET _____ GMS
E/C BLANK
(M) = 100 MLS

CORRECTED NET
(N) = K - (H) $\left(\frac{M}{100} \right)$
= _____ $\left(\frac{100}{100} \right)$
= _____ GMS
SCALED UP NET = (P) $\left(\frac{E}{G} \right)$
= _____ $\left(\frac{100}{100} \right)$
= _____ GMS

Particulates

NO. 1 FLOW AND MECHANICAL WEIGHT 10117 GRMS

0 021

NO. 2 FLOW AND MECHANICAL WEIGHT 10117 GRMS

NO. 3 FLOW AND MECHANICAL WEIGHT 10117 GRMS

NO. 4 FLOW AND MECHANICAL WEIGHT 10117 GRMS

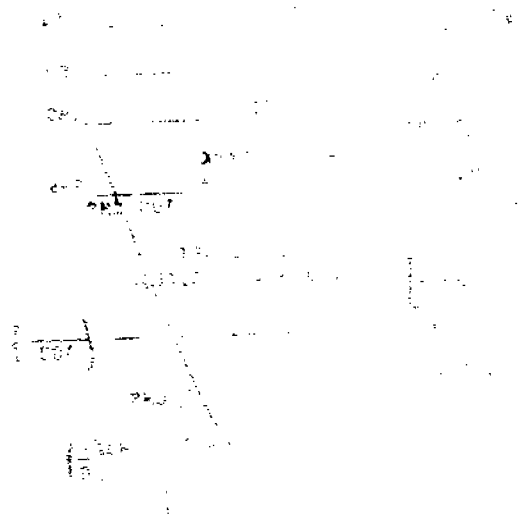
NO. 5 FLOW AND MECHANICAL WEIGHT 10117 GRMS

Totals

GRAINS/DSCF = 1.608752E-02

POUNDS/HOUR = .2805597

HIT RETURN TO CONTINUE



PARTICULATE FIELD DATA SHEET

PLANT Maxwell House DATE 1 RUN NO. 3
 SAMPLE LOCATION OUTLET RAC BOX NO. 4 DRY GAS METER NO. 175176
 NOZZLE NO. _____ NOZZLE SIZE 1/2 INCHES PITOT NO. 7 C_p .83
 TIME AT EACH POINT (S) 2 1/2 MINUTES DELTA H @ 2.00 THERMOCOUPLE NO.: 41
 AMBIENT PRESSURE (P_{BAR}) 29.80 "HG PROBE OUTLET 38
 BOX OUTLET 18
 STATIC PRESSURE (P) -0.02 "H₂O/13.6 = _____ "Hg(P meter)
 STACK PRESSURE (P_s) = P_{bar} + P_{meter} = _____ "Hg OPERATING CONDITION OR REMARKS _____
 DRY BULB _____ °F WET BULB _____ °F _____ %H₂O

PORT/ POINT	MILITARY CLOCK TIME	METER READING	PITOT DELTA P "H ₂ O	ORIFICE DELTA H "H ₂ O	METER TEMP. °F		LINE VAC "Hg	PROBE OUTLET °F	BOX OUTLET TEMP °F	BOX TEMP °F	STACK TEMP °F
					IN	OUT					
A-1	1045	189.263	.07	1.3	85	86	6+	189	192	209	1548
2	47 1/2	90.6	.065	1.2	86	85	6+	191	198	221	1543
3	50	92.1	.065	1.2	87	85	6+	193	200	225	1520
4	52 1/2	93.7	.07	1.3	89	85	6+	195	201	226	1530
5	55	95.7	.07	1.3	90	85	6+	198	203	225	1548
6	57 1/2	96.8	.07	1.3	90	85	6+	199	205	225	1548
7	1100	97.7	.065	1.2	91	85	6+	200	210	225	1546
8	02 1/2	99.5	.07	1.3	91	85	6+	201	211	226	1520
9	05	00.6	.065	1.2	92	86	6+	202	210	223	1492
10	07 1/2	3.2	.065	1.2	94	86	6+	202	210	225	1522
11	10	4.3	.07	1.3	95	86	6+	203	212	228	1520
12	12 1/2	5.4	.04	.75	95	87	6+	204	213	228	1500
40	1115	206.770									
B-1	1135	207.6	.05	.94	90	87	5+	200	201	225	1580
2	3 1/2	208.5	.05	.94	91	87	5+	203	200	224	1571
3	220 40	209.73	.065	1.2	88	88	6+	200	200	226	1530
4	22 1/2	211.2	.065	1.2	88	87	6+	207	201	225	1565
5	25 40	211.8	.05	.94	90	87	5+	200	202	228	1533
6	27 1/2	212.0	.06	1.12	91	87	5+	201	203	227	1530
7	29 50	213.7	.06	1.12	92	87	5+	202	204	227	1500
8	32 40	215.6	.06	1.12	93	87	5+	203	204	225	1501
9	35 05	218.0	.07	1.3	94	88	6+	203	205	226	1498
10	37 1/2	219.2	.07	1.3	94	88	6+	203	205	225	1498
11	40 00	220.0	.065	1.2	95	88	6+	203	205	228	1494
12	42 1/2	221.9	.065	1.2	95	88	6+	203	205	227	1495
END	46 12 43	223.470									
9	46 00										

* Sum, average or Difference

Pre-Leak Check 0.01 at 15" Post Leak Check ✓FYRITE: % OXYGEN 15.0
% CARBON DIOXIDE 5.0Tent
stop
at 11:14
Resum
work
12:2
Finis
12:4

SECTION 1: AVERAGE VELOCITY

Date: 12/11/07

Time: 10:10 AM

AVERAGE VELOCITY PRESSURE

Delta P in H ₂ O	Delta P square root
0.07	0.26
0.07	0.25
0.07	0.25
0.07	0.26
0.07	0.26
0.07	0.26
0.07	0.25
0.07	0.26
0.07	0.25
0.07	0.25
0.07	0.26
0.04	0.20
0.03	0.22
0.03	0.22
0.07	0.25
0.07	0.25
0.03	0.22
0.06	0.24
0.06	0.24
0.06	0.24
0.07	0.26
0.07	0.26
0.07	0.25
0.07	0.25

THE AVERAGE SQUARE ROOT OF DELTA P = .2507011

0 094

CLIENT: MAXWELL JOUSE

Date: 02/26/89

Time: 10:35 AM

Delta H (IN H ₂ O)	Meter Temp (F)		Stack Temp (F)
	IN	OUT	
1.20	86.00	86.00	1548.00
1.20	86.00	86.00	1548.00
1.20	87.00	85.00	1520.00
1.30	87.00	85.00	1530.00
1.30	90.00	85.00	1548.00
1.30	90.00	85.00	1548.00
1.20	91.00	85.00	1548.00
1.30	91.00	85.00	1520.00
1.20	92.00	86.00	1492.00
1.20	94.00	86.00	1522.00
1.30	95.00	86.00	1520.00
0.75	95.00	87.00	1500.00
0.94	90.00	87.00	1580.00
0.94	91.00	87.00	1571.00
1.20	88.00	88.00	1530.00
1.20	88.00	87.00	1565.00
0.94	90.00	87.00	1535.00
1.12	91.00	87.00	1530.00
1.12	92.00	87.00	1500.00
1.12	93.00	87.00	1501.00
1.30	94.00	88.00	1498.00
1.30	94.00	88.00	1498.00
1.20	95.00	88.00	1494.00
1.20	95.00	88.00	1495.00

AVERAGESDELTA H = 1.172064 IN H₂O

METER TEMP. = 88.79166 F

STACK TEMP. = 1526.355 F

SAMPLE LOCATION

Outlet

HYDROCARBON SAMPLING DATA

RUN NO.

1

DATE

2/1/89

0 025

HYDROCARBON PUMP NO.

TIME	ROTAMETER SETTING	GAS METER TEMP.	VACUUM "HG	SAMPLE RATE L/M
1045	60	80	17	1
50	60	81	17	1
55	60	82	17	1
1100	60	84	17	1
05	60	84	17	1
10	60	84	17	1
15	60	84	17	1
20	60	85	17	1
25	60	85	17	1
30	60	86	17	1
35	60	87	17	1
40	60	88	17	1
1145	60	88	17	1

PRE-LEAK CHECK

✓

POST-LEAK CHECK

✓

PUMP CALIBRATION FLOW RATE		CALIBRATION INSTRUMENT	TYPIE
FLOW RATE	ROTAMETER	SOAP FILM BURET	% OXYGEN
LITERS/MIN	SETTING	DRY GAS METER	% CARBON DIOXIDE
		OTHER	

CORRECTING ROTAMETER VOLUME TO DRY STANDARD CONDITIONS

$$\text{EQUATION: } V_{\text{STD}} = V_m \times \frac{P_m}{T_m} \times \frac{T_{\text{STD}}}{P_{\text{STD}}}$$

WHERE:

 V_m = SAMPLE RATE OF ROTAMETER (L/M) T_{STD} = $70^{\circ}\text{F} + 460^{\circ}\text{F} = 530^{\circ}\text{F}$ P_{STD} = 29.92"HG P_m = BAROMETRIC PRESSURE DURING SAMPLING ("HG) T_m = TEMPERATURE OF GAS STREAM (+460°F)

$$V_{\text{STD}} = \quad \times \left(\frac{\quad}{\quad} \right) \times \frac{(530)}{(29.92)} = \quad$$

$$\text{CF} = (V_{\text{STD}} \text{ L/MIN}) (3.53 \times 10^{-2} \text{ CF/L}) (60 \text{ MIN/1 HR}) = (\quad) (3.53 \times 10^{-2}) (60)$$

= CFH

PARTICULATE ATG (AUGUST 1988)

AirRecon
THREE BRIDGES, NJ

Method #3 Gas Bag and Impinger Contents Data Sheet

Company Name: MAXWELL HOUSE Total Wet Catch(mls): 44.00
 Unit: AFTERBURNER OUTLET Sample Volume(std. Ft3): 2.12
 Loc at. Site: HOBOKEN, NJ Stack Flowrate(DSCFM): 1930.00
 Run #: 3 Stack % Moisture: 9.30
 Date: 11-11-87
 Site: 11-11-87

Contaminants	Name	MW	GC: Liquid	GC: Gas
			Concentration (mg/l)	Concentration (ppmv)
(1)	THC as METHANE	16.04	0.000	30.000
(2)	CARBON MONOXIDE	28.01	0.000	166.000
(3)				
(4)				
(5)				
(6)				
(7)				
(8)				
(9)				
(10)				

Concentrations and Emissions				
Contaminants	Name	LB/HR	PPMV(WET)	PPMV(DRY)
(1)	THC as METHANE	0.147	27.810	30.662
(2)	CARBON MONOXIDE	1.391	150.562	166.000
(3)		0.000	ERR	ERR
(4)		0.000	ERR	ERR
(5)		0.000	ERR	ERR
(6)		0.000	ERR	ERR
(7)		0.000	ERR	ERR
(8)		0.000	ERR	ERR
(9)		0.000	ERR	ERR
(10)		0.000	ERR	ERR

This Program Uses the Following Equations for Each Contaminant Where:

W = Total Wet Catch (mls)
 V = Sample Volume (std. Ft3)
 M = Stack Moisture (%)
 Q = Stack Flowrate (DSCFM)
 E = GC: Liquid Concentration (mg/l)
 F = GC: Gas Concentration (dry ppmv)
 G = Contaminant's Molecular Weight

For the Impinger Contents:

$(H1)$ = dry ppmv = $(E/16.013 \times W/V \times 10) + (F/16.013 \times W/V)$
 $(J1)$ = wet ppmv = $(dry\ ppmv) \times (100 - M) / 100$
 $(K1)$ = pounds/hour = $(dry\ ppmv/16.013 \times W/V \times 10) \times (G)$

For the Gas Bag Contents:

$(H2)$ = dry ppmv = (F)
 $(J2)$ = wet ppmv = $(dry\ ppmv) \times (100 - M) / 100$
 $(K2)$ = pounds/hour = $(0.00000015005 \times (dry\ ppmv) \times (V) \times (G))$

Concentrations and Emissions:

total dry ppmv = $(H1) + (H2)$
 total wet ppmv = $(J1) + (J2)$
 total pounds/hour = $(K1) + (K2)$

MOISTURE DETERMINATION

SAMPLE LOCATION outlet

RUN NO. 3

DATE 2-1-89

CHAIN-OF-CUSTODY SAMPLE NO. _____

	GRAMS
IMPINGER 1	FINAL WEIGHT <u>757.6</u> INITIAL WEIGHT <u>121.3</u> INCREASE
IMPINGER 2	FINAL WEIGHT <u>694.9</u> INITIAL WEIGHT <u>676.9</u> INCREASE
IMPINGER 3	FINAL WEIGHT <u>492.5</u> INITIAL WEIGHT <u>489.0</u> INCREASE
SILICA GEL	FINAL WEIGHT <u>749.7</u> INITIAL WEIGHT <u>732.6</u> INCREASE

	GRAMS
IMPINGER 1	<u>36.3</u>
IMPINGER 2	<u>18.0</u>
IMPINGER 3	<u>3.5</u>
SILICA GEL	<u>17.1</u>

TOTAL MASS OF WATER CAUGHT

69.9 GRAMS

CHAIN-OF-CUSTODY SAMPLE NO. _____

FILTER DIAMETER 4 INCHES

FILTER TYPE Glass Fib

FILTER: FINAL WEIGHT .6271 GMS
INITIAL WEIGHT .2171 GMS
INCREASE

0.0094 GRAMS

TOTAL MASS OF PARTICULATE CAUGHT THIS FILTER

IS ICE PRESENT IN THE IMPINGER BATH AT THE END OF THIS SAMPLE? YES _____ NO _____

CALCULATIONS

$$V_{m-std} = 17.65 (V_m) \left(\frac{P_{bar} + \Delta H / 13.6}{T_m + 460} \right) = 17.65 () \left(\frac{ + 13.6 }{ } \right)$$

$$= 17.65 () () = \text{_____} \text{ FT}^3$$

$$V_{w-std} (H_2O) = \frac{\text{GRAMS COLLECTED}}{21.2 \text{ GRAMS/FT}^3} = \frac{()}{(21.2)} = \text{_____} \text{ FT}^3$$

$$\% H_2O = \frac{(V_{w-std}) 100}{((V_{w-std}) + (V_{m-std}))} = \frac{100 ()}{() ()} = \frac{()}{()} = \text{_____} \%$$

$$\text{MOLECULAR WEIGHT (MW)} = \frac{18 (\% H_2O)}{100} + \frac{\text{DRY MW} (100 - \% H_2O)}{100} = 0.18 () + \frac{() ()}{100}$$

$$\text{VELOCITY (ACTUAL) IN STACK} = 85.48 (Cp) \sqrt{\frac{T_s + 460}{P_s (MW)}} \sqrt{\Delta P} = 85.48 () \sqrt{\frac{()}{() ()}} \sqrt{\Delta P}$$

$$V_s = () \sqrt{\Delta P} = () () \sqrt{\Delta P}$$

$$V_s = () \Delta P = () () = \text{_____} \text{ FT/SEC}$$

$$ACFM = (V_s)(60)(CSA) = () (60) () = \text{_____}$$

$$\text{VELOCITY @ Stp } V_{s-std} = V_s (17.65) \left(\frac{P_s}{T_s + 460} \right) = \frac{() (17.65) ()}{()} = \text{_____} \text{ FT/SEC}$$

$$SCFM = (V_{s-std})(CSA)(60) = () () (60) = \text{_____}$$

$$DSCFM = \left(\frac{100 - \% H_2O}{100} \right) (SCFM) = () () = \text{_____}$$

$$\text{NOZZLE VELOCITY @ STD } V_n = \frac{(V_{m-std} + V_{w-std})}{60 (8) A_n} = \frac{()}{60 () () (10^{-4})} = \text{_____} \text{ FT/SEC}$$

$$I = \frac{100 V_{n-std}}{V_{s-std}} = \frac{100 ()}{()} = \text{_____} \% \text{ Isokinetic}$$

LAB DATA - EVAPORATIONS

PLANT MAXWELL HOUSESAMPLE LOCATION IntletRUN NO. 3 FOR _____SAMPLING DATE 2/1/89

OPERATING CONDITION _____

CHAIN-OF-CUSTODY SAMPLE NO. _____

ACETONE WASHINGS

GROSS 646.1 GMS
 TOTAL TARE - 455.6 GMS
 SAMPLE (A) NET 190.5 GMS
 AMOUNT EVAPORATED (B) 190.5 GMS
 EVAP. BEAKER NO. _____
 GROSS 96.8724 GMS
 TARE - 96.8665 GMS
 (C) NET 0.0059 GMS

ACETONE BLANK

EVAP. BEAKER NO. _____
99.6314 GROSS 96.8724 GMS
99.6316 TARE - 96.8665 GMS
0 NET 0.0059 GMS

ACETONE BLANK = NET 0 GMS (D)
 TOTAL AMOUNT
 EVAPORATED 100 GMS (F)

CORRECTED NET (E) = (C) - (B) $\left[\frac{(D)}{(F)} \right]$
 = (0.0059) - (190.5) $\left[\frac{0}{100} \right]$
 = 0.0059 GMS (E) = (C) - B $\left[\frac{(D)}{(F)} \right]$

SCALED UP NET = (E) $\left(\frac{A}{B} \right)$
 = 0.0059 $\left(\frac{190.5}{190.5} \right)$
 = 0.0059

WET CATCH

GROSS _____ GMS
 TOTAL TARE - _____ GMS
 SAMPLE (A) NET _____ GMS
 AMOUNT EXTRACTED (G) _____ GMS (MLS)
 AMOUNT OF E/O _____ GMS (H)

WATER PHASE
 EVAP. BEAKER NO. _____

GROSS _____ GMS
 TARE - _____ GMS
 (J) NET _____ GMS

WATER BLANK
 (L) = _____ GMS
100 GMS

CORRECTED NET
 (N) = J - (G)(L)
 = _____ $\left(\frac{100}{100} \right)$
 = _____ GMS

SCALED UP NET = (N) $\left(\frac{E}{G} \right)$
 = _____ $\left(\frac{190.5}{190.5} \right)$
 = _____ GMS

EC PHASE
 EVAP. BEAKER NO. _____

GROSS _____ GMS
 TARE - _____ GMS
 (K) NET _____ GMS

EC BLANK
 (M) = _____ GMS
100 MLS

CORRECTED NET
 (N) = K - (H)(M)
 = _____ $\left(\frac{100}{100} \right)$
 = _____ GMS

SCALED UP NET = (P) $\left(\frac{E}{G} \right)$
 = _____ $\left(\frac{190.5}{190.5} \right)$
 = _____ GMS

† *Journal of the American Statistical Association*, 1991, 86(414), 101-112.

NUMBER FILED 0 41 113

OF 12110. RELEASE 10 11 1955

totalis

GRAINS/DSCF = 7.354968E-03,

FULLNAME/HOUK = 1216771

FILE RETURN TO CONTINUE

CLIENT: SHAWWELL HOUSE

Date: 02/26/89

Time: 10:33 AM

THE FOLLOWING WERE PROGRAMMER INPUTS FOR ISOKINETICS

SAMPLE NO.	1	2	3
DATE	1/31/89	2/1/89	2/20/89
TIME	1000-1101	0700-0920	1045-1240
UNIT SAMPLED	OUTLET	OUTLET	OUTLET
ACTUAL NOZZLE DIAMETER (INCH), IN	0.50	0.50	0.50
PITOT FACTOR (CFM)	0.83	0.83	0.83
TIME @ EACH POINT (MIN)	3.00	2.00	2.00
AMBIENT PRESSURE (PSIA), (PSIA)	29.73	29.78	29.80
BARO. PRESSURE (PSIA), (PSIA)	+0.02	+0.02	+0.02
METER VOLUME (CM), (CM)	39.46	35.26	33.37
WATER COLLECTED/ INFLINGERS, GMS	67.30	56.70	69.90
CARBON DIOXIDE (CO ₂), %	6.70	6.30	6.00
OXYGEN (O ₂), %	13.20	13.10	14.00
STACK DIAMETER (INCH), IN	30.00	30.00	30.00
STACK LEAKS DETECTED/ PERCENT, (%)	4.91	4.71	4.91

CLIENT: MAXWELL HOUSE

Date: 02/26/89

Time: 10:38 AM

ISOKINETIC CALCULATIONS

SAMPLE NO.	1	2	3
DATE	1/31/89	2/1/89	2/20/89
TIME	0900-1104	0700-0920	1000-1030
UNIT SAMPLED	OUTLET	OUTLET	OUTLET
METER VOLUME (VM-STD) - SCFH	36.43	33.67	32.10
WATER COLLECTED (VM-STD) - SCFH	3.26	2.70	3.00
MOISTURE (VOL %)	7.60	7.62	9.34
ACTUAL MOLECULAR WEIGHT (MW), LBS/LB-POLE	28.69	28.60	28.40
ACTUAL VELOCITY IN STACK (VS), FT/SEC	27.54	27.98	27.21
ACTUAL FLOW RATE IN STACK (ACFM)	8112.98	8243.16	8017.09
VELOCITY @ STP (VS-STD), FT/SEC	7.42	7.48	7.23
STACK FLOW RATE @ STP (SCFM)	2184.81	2202.52	2129.38
DRY FLOW RATE (DSCFM)	2015.00	2034.63	1930.43
NOZZLE VELOCITY @ STP (VN-STD), FT/SEC	7.06	7.40	7.21
ISOKINETIC %	95.48	97.32	99.80

RECON SYSTEMS, INC.

Route 202 North, P.O., Box 460

Three Bridges, N.J. 08887

201-782-5900

LABORATORY ORSAT OR GC GAS ANALYSIS

0 102

PLANT General Foods - Maxwell House Division STACK Afterburner Inlet/Outlet

SAMPLE NO. _____ OPERATING CONDITIONS _____

JOB NO. 0641

--Dry Basis--

Sample ID	Date	% CO ₂	% O ₂	% CO	% N ₂ (By Diff.)
Run #1 Inlet	1/31/89	0.0	21.0	—	81.4
Sample ID	Date	% CO ₂	% O ₂	% CO	% N ₂ (By Diff.)
Run #2 Inlet	2/1/89	0.0	21.0	—	81.1
Sample ID	Date	% CO ₂	% O ₂	% CO	% N ₂ (By Diff.)
Run #3 Inlet	2/1/89	0.0	21.0	—	80.0
Sample ID	Date	% CO ₂	% O ₂	% CO	% N ₂ (By Diff.)
Run #1 Outlet	1/31/89	5.4	13.2	—	81.4
Sample ID	Date	% CO ₂	% O ₂	% CO	% N ₂ (By Diff.)
Run #2 Outlet	2/1/89	5.8	13.1	—	81.1
Sample ID	Date	% CO ₂	% O ₂	% CO	% N ₂ (By Diff.)
Run #3 Outlet	2/1/89	6.0	14.0	—	80.0
Sample ID	Date	% CO ₂	% O ₂	% CO	% N ₂ (By Diff.)

CHEMIST: Bob F. Mudd

Date: 2/2/89

L-18 (8.17.82)

ENGINEERING, CONSULTING, LABORATORY,
PILOT PLANT, PLANT TEST SERVICES

POLLUTION CONTROL, WASTE DISPOSAL,
RESOURCE RECOVERY, CHEMICAL PROCESS SYSTEMS

Linear Regression Calculations
for Gas Chromatographic Analysis - Impingers

RECON SYSTEMS INC
THREE BRIDGES, NJ

STANDARDS		UNKNOWN					
Conc. (mg/L)	Area Counts	Sample ID	Sample Number	Sample Area Counts	Dil. Factor	Dil. Samp. Conc. (mg/L)	Actual Conc. (mg/L)
0	10792	Outlet-1	14568	13447	1.00	1.0	1.0
11.69	43194	Outlet-2	14569	12368	1.00	0.6	0.6
23.38	76859	Outlet-3	14570	9836	1.00	-0.3	ND

Method Detection Limit - 0.5 ug/L

Client: General Foods/Maxwell House
Job Number: 0641

Compound: Total HxCx (as Methane)
Sample Location: Afterburner Outlet
Sample Date: 1-/31,2/1,1989

Report Date: 08-Feb-89

Samples Run: 3

Analyst: RNS

Reference: RNS83, p.32

2mL inj. of samples and standards.

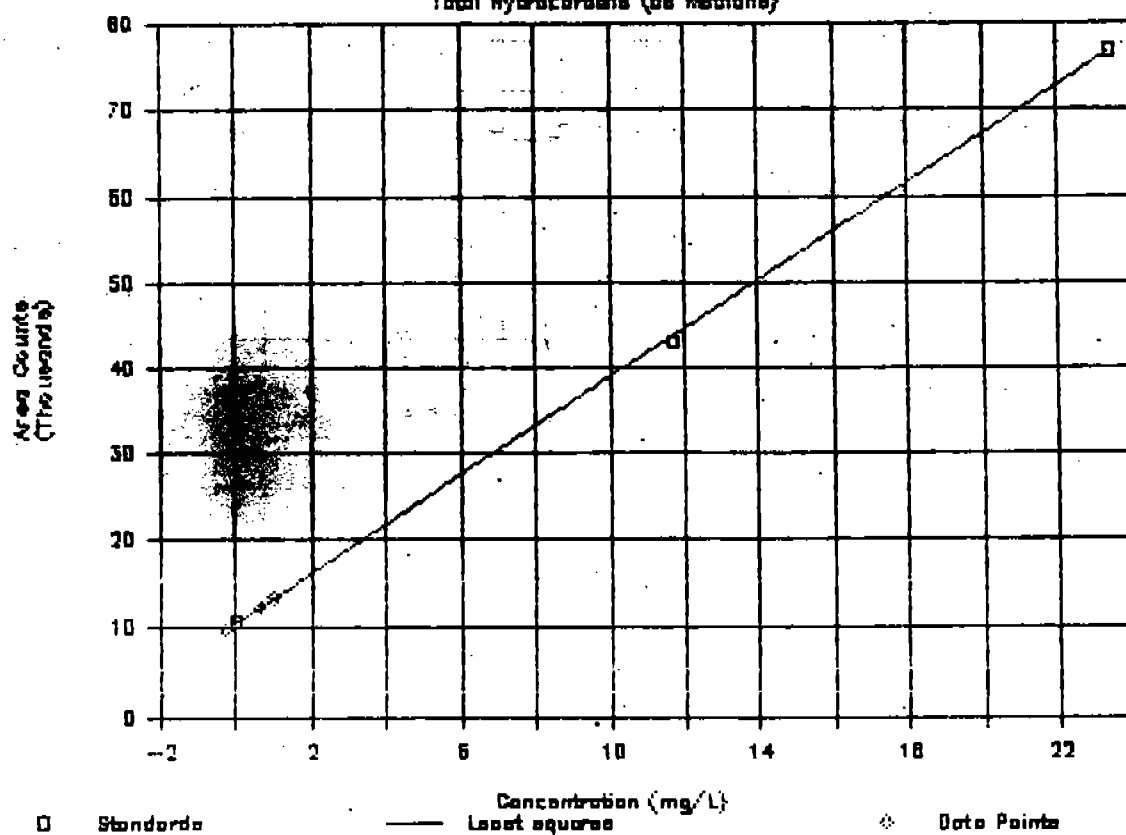
Total volume of 44 mL.

COEFF. OF DETERMIN.
0.9998781

COEFF. OF CORRELATION
0.9999390

STD ERROR OF ESTIMATE
5.157E+02

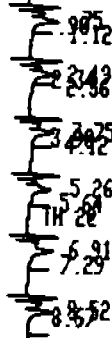
Gas Chromatographic Analysis
Total Hydrocarbons (as Methane)



ID 0.00

Blank H₂O

START



STOP

RUN # 18
ID 0.0

FEB/07/89 12:14:08

AREAZ

RT	AREA	TYPE	AR/HT	AREAZ
0.75	3698	D BP	0.067	4.890
0.90	2375	PV	0.083	3.141
1.12	8517	D VB	0.178	11.263
2.19	4360	D BP	0.072	5.766
2.34	1796	PV	0.089	2.375
2.56	6935	VB	0.164	9.171
3.75	3955	D BP	0.069	5.230
3.90	2033	PV	0.097	2.689
4.12	7722	VB	0.185	10.212
5.26	4139	D BP	0.077	5.474
5.64	7260	VB	0.186	9.601
6.91	4165	D BP	0.073	5.508
7.29	11120	PB	0.228	14.706
8.52	3593	D BP	0.066	4.752
8.67	3950	PV	0.129	5.224

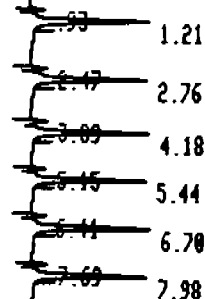
TOTAL AREA= 75618
MUL FACTOR= 1.0000E+00

LIST: ID 1

11.69 mg/L as Methane

0 100

START



STOP

RUN # 20
ID 1

FEB/07/89 12:37:06

AREAZ

RT	AREA	TYPE	AR/HT	AREAZ
0.93	3569	D BP	0.065	1.269
1.21	45058	D PB	0.106	16.024
2.47	3918	D BP	0.071	2.1393
2.76	45830	D PB	0.110	16.298
3.89	3828	D PP	0.070	1.379
4.18	43384	D PB	0.101	15.428
5.15	4063	D BP	0.074	1.445
5.44	40224	D PB	0.098	14.322
6.41	4221	D BP	0.071	1.554
6.70	43003	D PB	0.101	15.293
7.69	3673	D BP	0.066	1.306
7.98	40178	D PB	0.098	14.288

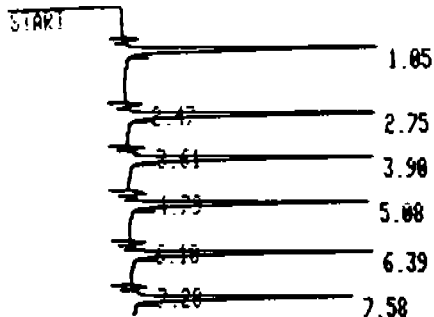
TOTAL AREA= 281200
MUL FACTOR= 1.0000E+00

23.38mg/L as CH₄

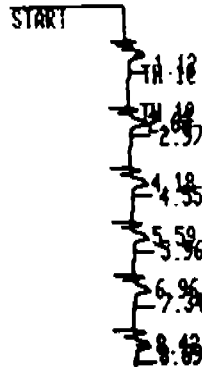
0 107

ID 14568-0641e

ID 2e



STOP



STOP

RUN # 24
ID 2

FEB/07/89 13:19:07

RUN # 4
ID 14568-0641

FEB/07/89 10:49:50

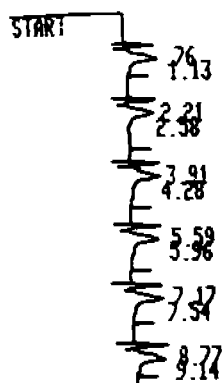
AREA%	RT	AREA	TYPE	AR/HT	AREA%
1.05	X79734	D	PB	0.089	16.610
2.47	4468	D	BP	0.069	0.931
2.75	84914	D	PB	0.096	17.689
3.61	4225	D	BP	0.068	0.880
3.98	X78863	D	PB	0.089	16.262
4.79	3963	D	PP	0.067	0.826
5.08	X73968	D	VB	0.087	15.409
6.10	4013	D	BP	0.068	0.836
6.39	X75670	D	VB	0.088	15.763
7.28	3441	D	BP	0.067	0.717
7.58	67585	D	PB	0.086	14.079

TOTAL AREA= 480040
MUL FACTOR= 1.0000E+00

AREA%	RT	AREA	TYPE	AR/HT	AREA%
1.12	5124	VV		0.095	6.501
2.60	2747	D	BP	0.071	3.485
2.97	X13567	PB		0.201	17.212
4.18	3111	D	BP	0.073	3.947
4.55	X13179	PB		0.223	16.719
5.59	3118	D	BP	0.073	3.956
5.96	X13272	PB		0.224	16.837
6.96	2898	D	BP	0.072	3.677
7.34	X13771	PB		0.240	17.470
8.42	2754	D	BP	0.070	3.494
8.69	5204	PV		0.110	6.704

TOTAL AREA= 78825
MUL FACTOR= 1.0000E+00

ID 14569-0641e



STOP

RUN # 19
ID 14569-0641

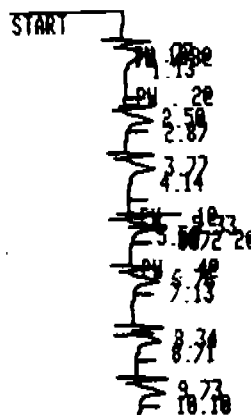
FEB/07/89 12:26:00

RT	AREA	TYPE	AR/HT	AREA*
0.76	3283	D BP	0.066	3.418
1.13	X12289	PB	0.223	12.793
2.21	3734	D BP	0.071	3.887
2.58	10680	PB	0.220	11.118
3.91	3545	D BP	0.067	3.690
4.28	13274	PB	0.237	13.818
5.59	4145	D BP	0.076	4.315
5.96	11070	PB	0.221	11.524
7.17	3931	D BP	0.067	4.092
7.54	13825	PB	0.224	13.559
8.77	4639	D BP	0.074	4.829
9.14	X12446	PB	0.237	12.956

TOTAL AREA= 96861
MUL FACTOR= 1.0000E+00

LIST: ID 14570-0641

0 108



STOP

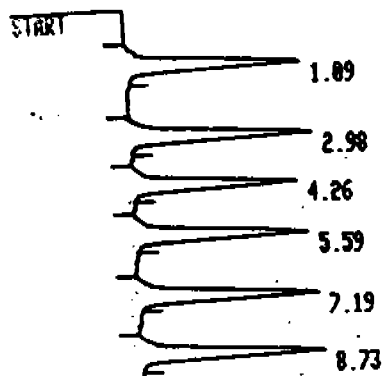
RUN # 17
ID 14570-0641

FEB/07/89 12:01:00

RT	AREA	TYPE	AR/HT	AREA*
0.77	3727	D BP	0.070	3.946
1.13	[14958	D PB	0.414	15.836
2.58	2129	D BP	0.055	2.265
2.87	X[9460	PB	0.191	10.015
3.77	3897	D BP	0.072	4.126
4.14	[13143	PB	0.236	13.914
5.33	3495	BB	0.039	3.700
5.59	X	PB	0.000	0.000
5.72	1366	D BB	0.034	1.446
6.76	4314	D BP	0.075	4.567
7.13	X[9855	PB	0.199	10.433
8.34	3535	D BB	0.066	3.742
8.71	X[9422	BB	0.207	9.975
9.73	4541	D BP	0.075	4.808
10.10	X[10605	PB	0.210	11.227

TOTAL AREA= 94457
MUL FACTOR= 1.0000E+00

Post-cal check 23.38 mg/L as Methane
 ID 2 e ~~24.21 mg/L as Hexane~~



STOP

RUN # 37
 ID 2

FEB/07/89 15:10:14

AREA%	RT	AREA TYPE	AR/HT	AREA%
	1.09	X86348 D PB	0.269	16.581
	2.98	X86348 D PB	0.274	17.456
	4.26	X78936 D PB	0.264	15.158
	5.59	X83675 D PB	0.266	16.068
	7.19	X86348 D PB	0.269	16.943
	8.73	X86348 D PB	0.290	17.795

Average Area C₂₅ = 22986

TOTAL AREA= 520770
 MUL FACTOR= 1.0000E+00

RECON SYSTEMS, INC.
ROUTE 202N, BOX 460, THREE BRIDGES, NJ 08887
201-782-5900

0 110

CHAIN-OF-CUSTODY/REQUEST FOR ANALYSIS/DOT SHIPPING PAPER

(Use one form for each sample)

PROJECT MANAGER PFM

SAMPLE NO. D 14568 ANALYTICAL RESULTS TO BE REPORTED TO: PFM

SAMPLE LOCATION afterburner outlet Run 1 RECON JOB NO. 0641

SAMPLE DESCRIP. voc vial 40ml SAMPLING DATE/TIME 1-31-89 BY: CDR/PM

Relinquished By Person/Organ. (Signature)	Received By Person/Organ./ Date/Time (Signature)	Container Description and Preservative	Analysis Requested	Analysis Performed By Person/Lab	Date/Time Analysis Performed	Results
SJC	Rod/Rec 2-2-89 11:03	40ml vial	Total Hydrocarbons	ANS /R	2-2-89	

MAKE ADDITIONAL COMMENTS/NOTES

RUSH

YES NO

☐ ☒

EMERGENCY

YES NO

☐ ☒

COMPLIANCE OR TIER II

YES

☒

IF SAMPLES HAVE BEEN DETERMINED HAZARDOUS, PLEASE INCLUDE SHIPPING NAME, HAZARD CLASS, AND IDENTIFICATION NUMBER.

RECON SYSTEMS, INC.
ROUTE 202N, BOX 460, THREE BRIDGES, NJ 08887
201-782-5900

CHAIN-OF-CUSTODY/REQUEST FOR ANALYSIS/DOT SHIPPING PAPER

(Use one for sample) PROJECT MANAGER PFM
SAMPLE NO. 0 14569 ANALYTICAL RESULTS TO BE REPORTED TO: PFM
SAMPLE LOCATION qfforner outlet Run 2 RECON JOB NO. 0641
SAMPLE DESCRIPT. 40ml voc vial SAMPLING DATE/TIME 2-1-89 10:00 BY: ODE/PM

Relinquished By Person/Organ. (Signature)	Received By Person/Organ./ (Signature)	Container Description and Preservative	Analysis Requested	Analysis Performed By Person/Lab	Date/Time Analysis Performed	Results
STC	<u>Rolls/Rec</u> <u>2-2-89</u> <u>11:06</u>	<u>40ml voc vial</u>	<u>Total hydrocarbons</u>	<u>ANS/PE</u>	<u>2-7-89</u>	

MAKE ADDITIONAL COMMENTS/NOTES _____

RUSH ☐ YES ☒ NO

EMERGENCY ☐ YES ☒ NO

COMPLIANCE OR TIER II ☒ YES

IF SAMPLES HAVE BEEN DETERMINED HAZARDOUS, PLEASE INCLUDE SHIPPING NAME, HAZARD CLASS, AND IDENTIFICATION NUMBER.

RECON SYSTEMS, INC.
ROUTE 202N, BOX 460, THREE BRIDGES, NJ 08887
201-782-5900

CHAIN-OF-CUSTODY/REQUEST FOR ANALYSIS/DOT SHIPPING PAPER

(Use one form sample) PROJECT MANAGER PFM

SAMPLE NO. D 14570 ANALYTICAL RESULTS TO BE REPORTED TO: PFM

SAMPLE LOCATION afterburner outlet run 3 RECON JOB NO. 0641

SAMPLE DESCRIPT. 40ml. voc vial SAMPLING DATE/TIME 2-1-89 11:09 BY: CDR/PM

Relinquished By Person/Organ. (Signature)	Received By Person/Organ./ Date/Time (Signature)	Container Description and Preservative	Analysis Requested	Analysis Performed By Person/Lab	Date/Time Analysis Performed	Results
SJC	<u>DD/Rec</u> <u>2-2-89</u> <u>11:09</u>	<u>40ml voc</u> <u>vial</u>	<u>total</u> <u>hydrocarbons</u>	<u>ANS/R</u>	<u>2-7-89</u>	

MAKE ADDITIONAL COMMENTS/NOTES _____

RUSH ☐ YES ☒ NO

EMERGENCY ☐ YES ☒ NO

COMPLIANCE OR TIER II ☒

IF SAMPLES HAVE BEEN DETERMINED HAZARDOUS, PLEASE INCLUDE SHIPPING NAME, HAZARD CLASS, AND IDENTIFICATION NUMBER.

CHAIN-OF-CUSTODY/REQUEST FOR ANALYSIS/DOT SHIPPING PAPER

(Use one for sample)

PROJECT MANAGER PFM

SAMPLE NO. B 14574 ANALYTICAL RESULTS TO BE REPORTED TO: PFM

SAMPLE LOCATION Blg K (Trip) RECON JOB NO. 0641

SAMPLE DESCRIPT. Water SAMPLING DATE/TIME BY: SR

Relinquished By Person/Organ. (Signature)	Received By Person/Organ./ Date/Time (Signature)	Container Description and Preservative	Analysis Requested	Analysis Performed By Person/Lab	Date/Time Analysis Performed	Results
SR	<u>SR/Rec</u> <u>2-2-89</u> <u>11:24</u>	<u>Distilled</u> <u>Water</u> <u>Blank</u>	<u>TOTAL</u> <u>Hydrocarbons</u>	<u>SR</u>		
<u>REVOKED</u>						

MAKE ADDITIONAL COMMENTS/NOTES

RUSH

YES NO

☐ ☒

EMERGENCY

YES NO

☐ ☒

YES

COMPLIANCE TIER II

☐

IF SAMPLES HAVE BEEN DETERMINED HAZARDOUS, PLEASE INCLUDE SHIPPING NAME, HAZARD CLASS, AND IDENTIFICATION NUMBER.

COPIES OF THIS FORM MUST BE ATTACHED TO EACH LABORATORY REPORT.

L-37A (CPB)(July 11, 1988)

RECON SYSTEMS INC.

ROUTE 202N, P.O. BOX 460, THREE BRIDGES, N.J. 08887-0460
201-782-5000 FAX 201-782-0072

NEW ENGLAND 508-752-4222 PENNSYLVANIA 215-433-5511 CONNECTICUT 203-293-1212

ANALYSIS REPORT

February 14, 1989

TO: Maxwell House/General Foods Project Attn: P. F. Marshall
RECON Project No. 0641

Sample: 80 Liter Tedlar Gas Bag; sampled 1/31/89

RECON Sample No.	RUN NO.	SAMPLE DESCRIPTION	OXYGEN (%)	CO PPMV DRY	THC AS METHANE PPMV DRY
14571	1	OUTLET	13.2	131	19.
14572	2	OUTLET	13.1	416	35.
14573	3	OUTLET	14.0	166	30.
Detection Limit			0.1	0.1	1

Samples from this project will be retained for sixty days from the date of this report unless directed otherwise.

Submitted by

Patrick J. Mulrooney
Patrick J. Mulrooney, B.S.
Acting Laboratory Director

Andrew W. McNeel
per Andrew W. McNeel, B.S.
Test Engineer

AWM/lej (AR16)
0641

New Jersey State Certified Water Laboratory
Certification No. 10196

RECON SYSTEMS, INC.
ROUTE 202N, BOX 460, THREE BRIDGES, NJ 08887
201-782-5900

CHAIN-OF-CUSTODY/REQUEST FOR ANALYSIS/DOT SHIPPING PAPER

(Use one form for each sample)

PROJECT MANAGER PJM

SAMPLE NO. D 14571 ANALYTICAL RESULTS TO BE REPORTED TO: PJM

SAMPLE LOCATION 9FT DEPTH OUTLET RUN 1 RECON JOB NO. 0641

SAMPLE DESCRIPT. 80L Tether Bag SAMPLING DATE/TIME 2-2-89 BY: LOD/PJM

Relinquished By	Received By	Container Description	Analysis Requested	Analysis Performed By	Date/Time	Analysis Results
Person/Organ. (Signature)	Person/Organ. (Signature)	and Preservative	Requested	Person/Lab	Performed	Results
SJC	<u>LOD/Rec</u> 2-2-89 11:12	80L Tether Bag	TOTAL hydrocarbon as methane carbon monoxide oxygen	<u>ALUM</u> 1R	2-2-89 1300	

MAKE ADDITIONAL COMMENTS/NOTES _____

RUSH ☐ YES ☒ NO

EMERGENCY ☐ YES ☒ NO

COMPLIANCE TIER II ☒

IF SAMPLES HAVE BEEN DETERMINED HAZARDOUS, PLEASE INCLUDE SHIPPING NAME, HAZARD CLASS, AND IDENTIFICATION NUMBER.

RECON SYSTEMS, INC.
ROUTE 202N, BOX 460, THREE BRIDGES, NJ 08887
201-782-5900

CHAIN-OF-CUSTODY/REQUEST FOR ANALYSIS/DOT SHIPPING PAPER

(Use one for: 1 sample)PROJECT MANAGER PFMSAMPLE NO. G 14572ANALYTICAL RESULTS TO BE REPORTED TO: PFMSAMPLE LOCATION after burner outlet Run 2 RECON JOB NO. 0641SAMPLE DESCRIPT. 80 L red bar Bag SAMPLING DATE/TIME 2-2-89 1200 BY: CDR/PM

Relinquished By Person/Organ. (Signature)	Received By Person/Organ./ Date/Time (Signature)	Container Description and Preservative	Analysis By Registered Person/Lab	Analysis Performed Date/Time Analysis Performed Results
SJC	Adh/Rec 2-2-89 11:15	80 L red bar Bag	Total Hydrocarbons as Petroleum Carbon Monoxide Oxygen AUMC/R 1/R 1/R	2-2-89 1200

MAKE ADDITIONAL COMMENTS/NOTES

RUSH ☐ YES ☒ NOEMERGENCY ☐ YES ☒ NOCOMPLIANCE OR TIER II ☒

IF SAMPLES HAVE BEEN DETERMINED HAZARDOUS: PLEASE INCLUDE SHIPPING NAME, HAZARD CLASS, AND IDENTIFICATION NUMBER.

CHAIN-OF-CUSTODY/REQUEST FOR ANALYSIS/DOT SHIPPING PAPER

(Use one form for each sample)

PROJECT MANAGER PJM

SAMPLE NO. B 14573 ANALYTICAL RESULTS TO BE REPORTED TO: PJM

SAMPLE LOCATION afterburner outlet Run 3 RECON JOB NO. 0641

SAMPLE DESCRIPT. 80L Tedlar bag SAMPLING DATE/TIME 2-2-89 BY: col/pjm

Relinquished By Person/Organ. (Signature)	Received By Person/Organ./ Date/Time (Signature)	Container Description and Preservative	Analysis Requested	Analysis Performed By Person/Lab	Date/Time Analysis Performed	Results
SJC	<u>col/Rec</u> <u>2-2-89</u> <u>11:18</u>	<u>80L Tedlar</u> <u>bag</u>	<u>Total hydrocarbons</u> <u>as methane</u> <u>Carbon monoxide</u> <u>oxygen</u>	<u>ALM/IR</u> <u>IR</u> <u>IR</u>	<u>2-2-89</u> <u>1300</u>	

MAKE ADDITIONAL COMMENTS/NOTES

RUSH ☐ YES ☒ NO

EMERGENCY ☐ YES ☒ NO

COMPLIANCE OR TIER II ☒ YES

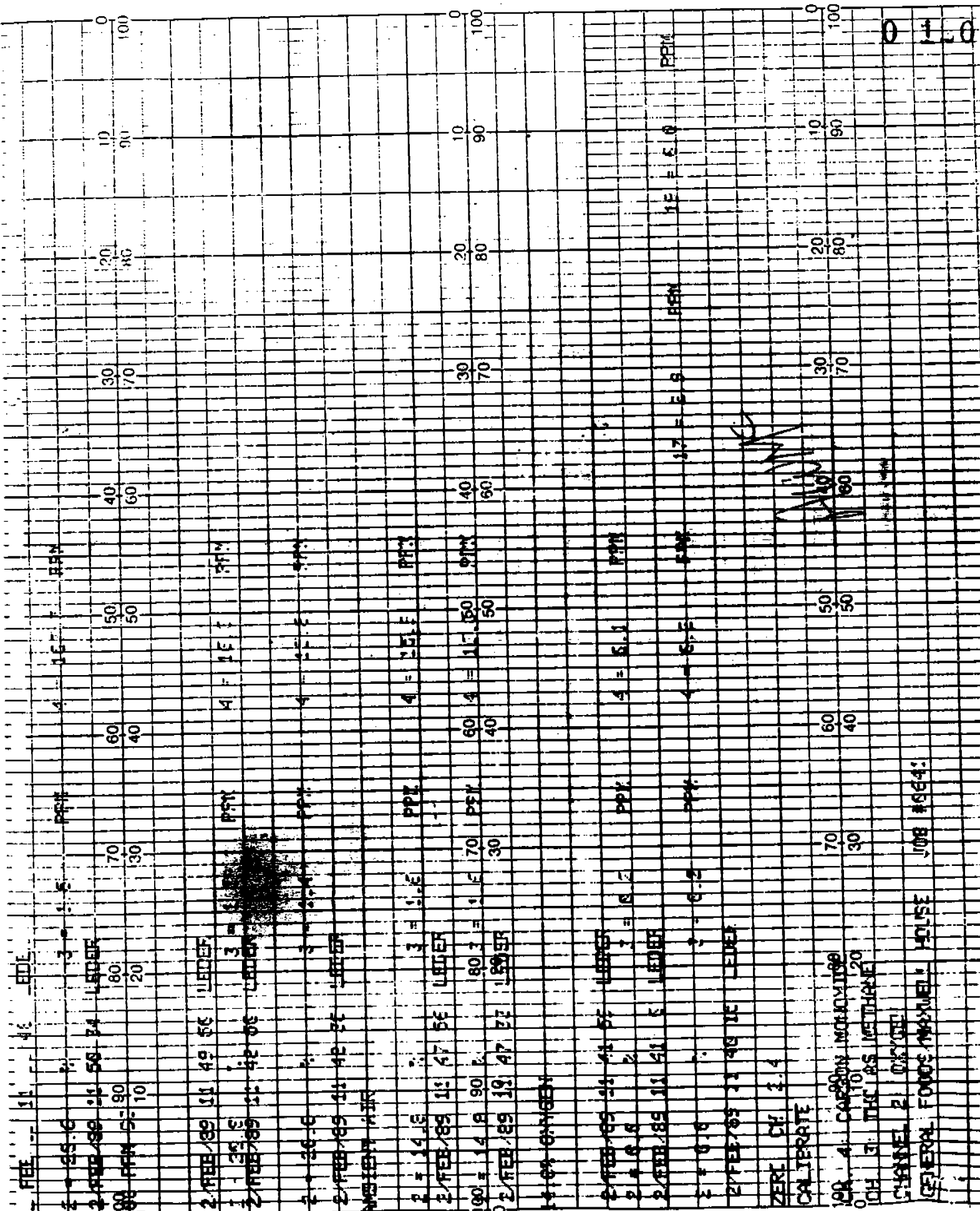
IF SAMPLES HAVE BEEN DETERMINED HAZARDOUS, PLEASE INCLUDE SHIPPING NAME, HAZARD CLASS, AND IDENTIFICATION NUMBER.

RATFISHE MODEL RS 55 FID OPERATING CONDITIONS

Sample pressure	<4 PSIG, Instrument 200 mbar
Fuel pressure	Regulator 15 PSIG, Instrument 0.3 bar
Zero gas pressure	Regulator 3PSIG
Span gas pressure	Regulator 3PSIG
Oven temperature	150°C
Combustion air	Regulator 15 PSIG, Instrument 0.8 bar

THERMO ELECTRON MODEL 48 NON-DISPERSIVE INFRARED,
GAS FILTER CORRELATION CO ANALYZER

Sample gas flow rate	1 LPM
Zero gas flow rate	1 LPM
Span gas flow rate	1 LPM
Sample conditioning	Filtration and Drying



100 PPM METHANE

100 = 14.8 90 = 80.3 = 5.7 70 PPM
0 = 10.0 10 = 20.3 = 1.7 30 PPM
2 FEB 89 12 23 17 LEADER

BAC SAMPLE LINE CHECK 14.8% O₂

2 = 15.5 PPM 3 = 792.8 PPM 4 = 11.1 PPM

3 FEB 89 12 14 4 LEADER

2 = 15.5 PPM 3 = 792.1 PPM 4 = 11.1 PPM

2 FEB 89 12 11 52 LEADER

2 = 15.5 PPM 3 = 792.5 PPM 4 = 11.1 PPM

2 FEB 89 12 11 52 LEADER

100 PPM METHANE

100 = 14.8 90 = 80.3 = 5.7 70 PPM
0 = 10.0 10 = 20.3 = 1.7 30 PPM
2 FEB 89 12 2 52 LEADER

2 = 15.5 PPM 3 = 80.7 PPM 4 = 11.1 PPM

2 FEB 89 12 2 36 LEADER

2 = 20.0 PPM 3 = 81.8 PPM 4 = 15.3 PPM

2 FEB 89 12 2 15 LEADER

2 = 20.0 PPM 3 = 81.8 PPM 4 = 15.3 PPM

100 PPM METHANE

100 = 14.8 90 = 80.3 = 5.7 70 PPM
0 = 10.0 10 = 20.3 = 1.7 30 PPM
2 FEB 89 12 5 42 LEADER

2 = 20.0 PPM 3 = 81.8 PPM 4 = 15.3 PPM

2 FEB 89 12 5 32 LEADER

2 = 20.0 PPM 3 = 81.8 PPM 4 = 15.3 PPM

2 FEB 89 12 5 22 LEADER

2 = 20.0 PPM 3 = 81.8 PPM 4 = 15.3 PPM

2 FEB 89 12 5 12 LEADER

2 = 20.0 PPM 3 = 81.8 PPM 4 = 15.3 PPM

2 FEB 89 12 5 2 LEADER

2 = 20.0 PPM 3 = 81.8 PPM 4 = 15.3 PPM

0 121