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Background Report Reference

AP-42 Section Number: 10.6.1

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**Title: Results Of The June 16, 1994
Particulate Emission Engineering
Test On The No. 1 And No. 2 Lines
At The Louisiana-Pacific Corp.
Facility Located In Hayward,
Wisconsin**

Interpoll Laboratories, Inc.

July 1994

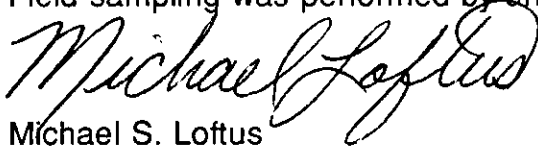
RESULTS OF THE JUNE 16, 1994
PARTICULATE EMISSION ENGINEERING TEST
ON THE NO. 1 AND NO. 2 LINES
AT THE LOUISIANA-PACIFIC CORPORATION FACILITY
LOCATED IN HAYWARD, WISCONSIN

Prepared For: Ms. Susan Somers
Louisiana-Pacific Corporation

Prepared By: PACE, Incorporated
1710 Douglas Drive North
Golden Valley, Minnesota 55422

PACE Project No.: 940614.401
Report Date: July 18, 1994

Field sampling was performed by and personnel under my direct supervision.



Michael S. Loftus
Project Field Supervisor

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EXECUTIVE SUMMARY

PACE Incorporated was contracted by Louisiana-Pacific Corporation to perform particulate emissions testing on the Line 1 and Line 2 dryers and EFB outlets at the Louisiana-Pacific facility located in Hayward, Wisconsin. This series of tests was performed on June 16, 1994.

Test Results Summary

Line 1

	<u>Test 1</u>		<u>Test 2</u>	
	EFB <u>Outlet</u>	Core Dryer <u>Outlet</u>	EFB <u>Outlet</u>	Surface Dryer <u>Outlet</u>
ACFM	95200	46200	93000	49300
DSCFM	50900	25300	51100	24200
Average Flue Gas Moisture Content (%v/v)	26.7	21.8	25.7	29.7
Average Flue Gas Temp. (°F)	242	246	235	247
Particulate Concentration (GR/DSCF)	0.108	0.201	0.094	0.301
Particulate Emission Factor (LB/KLB of Wet Flue Gas)	0.17	0.32	0.15	0.45
Particulate Removal Efficiency (%)		46.9		66.7

Line 2

	<u>Test 1</u>		<u>Test 2</u>	
	EFB <u>Outlet</u>	Core Dryer <u>Outlet</u>	EFB <u>Outlet</u>	Surface Dryer <u>Outlet</u>
ACFM	102600	50500	105800	56000
DSCFM	58200	29500	60600	31200
Average Flue Gas Moisture Content (%v/v)	22.5	18.2	21.7	22.5
Average Flue Gas Temp. (°F)	221	220	222	218
Particulate Concentration (GR/DSCF)	0.075	0.248	0.067	0.237
Particulate Emission Factor (LB/KLB of Wet Flue Gas)	0.12	0.41	0.11	0.38
Particulate Removal Efficiency (%)		70.7		71.1

INTRODUCTION

PACE, Incorporated personnel conducted particulate emission engineering testing on the line 1 and line 2 dryers and EFB outlets at the Louisiana-Pacific facility located in Hayward, Wisconsin. On-site testing was performed by a four member team consisting of M. Loftus, J. Pederson, K. Lattery and M. Wilson. Coordination between plant operations and testing activities was provided by Del Salquist of Louisiana-Pacific through direct contact with the test team leader. Testing was not witnessed by any representative with the Wisconsin Department of Natural Resources. The dryer outlet tests consisted of one independent one-hour samplings for particulate with concurrent integrated gas sampling for Orsat analyses. The EFB outlet tests consisted of two independent one-hour samplings for particulate with concurrent integrated gas samplings for Orsat analysis. An additional one-hour sampling (Test 3 Run 1) for particulate was performed on the EFB outlets and the sample was given to Del Salquist for independent constituent analysis.

The objectives of this project were to quantify particulate emissions and rate the amount going through the EFB.

Results are summarized in the next section followed by descriptions of the process under investigation and test methods. All supporting data are included in subsequent appendices.

RESULTS SUMMARY

Results of particulate determinations and gas composition are summarized in Tables 1-4.

Testing on Line 1 originally began on June 15, 1994. Problems were encountered with the process on Line 1 which resulted in re-testing on June 16th. After testing the Surface dryer on Line 1 process problems delayed the start of the testing on the Core dryer for 3 hours. A sample train power loss during the Core dryer test caused the static pressure of the duct to pull the filter off the holder. The test was ended 51.9 minutes into the run.

The test on the Line 2 Surface dryer lasted only 36 minutes, because the filter plugged on the dryer outlet. Both tests on the Line 2 EFB outlet were performed from the top port. the angle of the bottom port made it impossible to insert the probe into the duct.

No other problems were encountered in the sampling or analyses of emissions samples. On this and after complete review of the test results, we believe that the values reported herein are an accurate representation of the source conditions at the time of the test.

SUMMARY OF THE RESULTS

Louisiana - Pacific Corporation
Hayward, Wisconsin
PACE Project No. 940614.401

PACE Incorporated
June 22, 1994

TABLE 1
SUMMARY OF THE RESULTS

Line No. 1 EFB Outlet

Parameter	Run 2	Run 2	Average
Date of Run	6/16/94	6/16/94	
Time of Run	1135-1235	737-837	
Concurrently tested with	Core Dryer	Surface Dryer	
Volumetric Flow Rate			
ACFM	95200	93000	94100
DSCFM	50900	51100	51000
Gas Temperature (°F)	242	235	238
Gas Moisture Content (%v/v)	26.7	25.7	26.2
Gas Composition (%v/v,Dry)			
CO2	3.8	4.0	3.9
O2	17.0	16.9	17.0
N2	79.2	79.1	79.2
Isokinetic Variation (%)	105.1	105.1	
Particulate Emission Rate (LB/HR) *	47.2	41.2	44.2
Particulate Concentration *			
GR/ACF	0.058	0.052	0.055
GR/DSCF	0.108	0.094	0.101
Particulate Emission Factor *			
LB/KLB of Wet Flue Gas	0.17	0.15	0.16

*Dry catch plus organic and inorganic/residual wet catch

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PACE Incorporated
June 22, 1994

TABLE 2
SUMMARY OF THE RESULTS

Line No. 1 Dryers

Parameter	Core Dryer	Surface Dryer
Date of Run	6/16/94	6/16/94
Time of Run	1135-1327	735-836
Volumetric Flow Rate		
ACFM	46200	49300
DSCFM	25300	24200
Gas Temperature (°F)	246	247
Gas Moisture Content (%v/v)	21.8	29.7
Gas Composition (%v/v,Dry)		
CO2	3.8	4.0
O2	17.0	16.9
N2	79.2	79.1
Isokinetic Variation (%)	89.1	107.7
Particulate Emission Rate (LB/HR)*	43.7	62.4
Particulate Concentration*		
GR/ACF	0.110	0.148
GR/DSCF	0.201	0.301
Particulate Emission Factor*		
LB/KLB of Wet Flue Gas	0.32	0.45

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TABLE 3
SUMMARY OF THE RESULTS

Line No. 2 EFB Outlet

Parameter	Run 1	Run 1	Average
Date of Run	6/16/94	6/16/94	
Time of Run	1537-1637	1739-1818	
Concurrently tested with	Core Dryer	Surface Dryer	
Volumetric Flow Rate			
ACFM	102600	105800	104200
DSCFM	58200	60600	59400
Gas Temperature (°F)	221	222	221
Gas Moisture Content (%v/v)	22.5	21.7	22.1
Gas Composition (%v/v,Dry)			
CO2	2.2	2.8	2.5
O2	18.8	18.2	18.5
N2	79.0	79.0	79.0
Isokinetic Variation (%)	98.1	97.6	
Particulate Emission Rate (LB/HR) *	37.2	34.7	36.0
Particulate Concentration *			
GR/ACF	0.042	0.038	0.040
GR/DSCF	0.075	0.067	0.071
Particulate Emission Factor			
LB/KLB of Wet Flue Gas	0.12	0.11	0.11

*Dry catch plus organic and inorganic/residual wet catch

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TABLE 4
SUMMARY OF THE RESULTS

Line No. 2 Dryers

Parameter	Core Dryer Outlet	Surface Outlet
Date of Run	6/16/94	6/16/94
Time of Run	1537-1638	1737-1814
Volumetric Flow Rate		
ACFM	50500	56000
DSCFM	29500	31200
Gas Temperature (°F)	220	218
Gas Moisture Content (%v/v)	18.2	22.5
Gas Composition (%v/v,Dry)		
CO2	3.6	3.0
O2	17.6	18.0
N2	78.8	79.0
Isokinetic Variation (%)	96.3	101.4
Particulate Emission Rate (LB/HR) *	62.7	63.4
Particulate Concentration *		
GR/ACF	0.145	0.132
GR/DSCF	0.248	0.237
Particulate Emission Factor *		
LB/KLB of Wet Flue Gas	0.41	0.38

*Dry catch plus organic and inorganic/residual wet catch

RESULTS OF ORSAT AND MOISTURE DETERMINATIONS

TABLE 5
RESULTS OF ORSAT AND MOISTURE DETERMINATIONS

Line No. 1 EFB Outlet

Parameter	Run 2	Run 2
Date of Run	6/16/94	6/16/94
Time of Run	1135-1235	737-837
ORSAT (%v/v)		
Dry Basis		
Carbon Dioxide	3.80	4.00
Oxygen	17.00	16.90
Carbon Monoxide*	*	*
Nitrogen	79.20	79.10
WetBasis		
Carbon Dioxide	2.78	2.97
Oxygen	12.45	12.56
Carbon Monoxide*	*	*
Nitrogen	58.02	58.81
Portable Oxygen Monitor Result		
Time Weighted Average (%O2)		16.6
Moisture Collected (ml)	323.0	306.0
Moisture Content (%v/v)	26.75	25.65
Molecular Weight of Flue Gas (lb/lb-mole)		
Dry	29.29	29.32
Wet	26.27	26.41

*Carbon monoxide was not measured, assumed concentrations less than 0.01%.

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TABLE 6
RESULTS OF ORSAT AND MOISTURE DETERMINATIONS

Parameter	Line No. 1 Dryers	
	Core Dryer	Surface Dryer
Date of Run	6/16/94	6/16/94
Time of Run	1135-1327	735-836
ORSAT (%v/v)		
Dry Basis		
Carbon Dioxide	3.80	4.00
Oxygen	17.00	16.90
Carbon Monoxide*	*	*
Nitrogen	79.20	79.10
Wet Basis		
Carbon Dioxide	2.97	2.81
Oxygen	13.30	11.87
Carbon Monoxide*	*	*
Nitrogen	61.97	55.58
Portable Oxygen Monitor Result		
Time Weighted Average (%O ₂)	#DIV/0!	#DIV/0!
Moisture Collected (ml)	160.0	312.0
Moisture Content (%v/v)	21.76	29.74
Molecular Weight of Flue Gas (lb/lb-mole)		
Dry	29.29	29.32
Wet	26.83	25.95
Fo	1.026	1.000

*Carbon monoxide was not measured, assumed concentrations less than 0.01%.

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TABLE 7
RESULTS OF ORSAT AND MOISTURE DETERMINATIONS

Line No. 2 EFB Outlet

Parameter	Run 1	Run 1
Date of Run	6/16/94	6/16/94
Time of Run	1537-1637	1739-1818
ORSAT (%v/v)		
Dry Basis		
Carbon Dioxide	2.20	2.80
Oxygen	18.80	18.20
Carbon Monoxide*	.	.
Nitrogen	79.00	79.00
WetBasis		
Carbon Dioxide	1.70	2.19
Oxygen	14.56	14.25
Carbon Monoxide*	*	*
Nitrogen	61.19	61.86
Moisture Collected (ml)	284.0	182.0
Moisture Content (%v/v)	22.55	21.70
Molecular Weight of Flue Gas (lb/lb-mole)		
Dry	29.10	29.18
Wet	26.60	26.75

*Carbon monoxide was not measured, assumed concentrations less than 0.01%.

TABLE 8
RESULTS OF ORSAT AND MOISTURE DETERMINATIONS

Line No. 2 Dryers

Parameter	Core Dryer Outlet	Surface Outlet
Date of Run	6/16/94	6/16/94
Time of Run	1537-1638	1737-1814
ORSAT (%v/v)		
Dry Basis		
Carbon Dioxide	3.60	3.00
Oxygen	17.60	18.00
Carbon Monoxide*	.	.
Nitrogen	78.80	79.00
WetBasis		
Carbon Dioxide	2.94	2.32
Oxygen	14.39	13.95
Carbon Monoxide*	.	.
Nitrogen	64.43	61.22
Portable Oxygen Monitor Result		
Time Weighted Average (%O ₂)	17.6	18.1
Moisture Collected (ml)	185.0	161.0
Moisture Content (%v/v)	18.24	22.50
Molecular Weight of Flue Gas (lb/lb-mole)		
Dry	29.28	29.20
Wet	27.22	26.68

*Carbon monoxide was not measured, assumed concentrations less than 0.01%.

RESULTS OF PARTICULATE LOADING DETERMINATIONS

Louisiana - Pacific Corporation
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TABLE 9
RESULTS OF PARTICULATE LOADING DETERMINATIONS

Line No. 1 EFB Outlet

Parameter	Run 2	Run 2	
Date of Run	6/16/94	6/16/94	
Time of Run	1135-1235	737-837	
Sample Duration (Min.)	60.0	60.0	
Average Flue Gas Temperature (°F)	242.0	234.8	
Moisture Content of Flue Gas (%v/v)	26.75	25.65	
Particulate Collected (Mg)*			
Wet Catch	129.0	101.9	
Dry Catch	162.9	152.4	
Total	291.9	254.3	
Volumetric Flow Rate			
ACFM	95170	93030	
SCFM	69550	68690	
DSCFM	50950	51070	
Sample Volume (Cubic Feet)			
Meter Conditions	45.12	44.16	
Dry Standard	41.64	41.74	
Isokinetic Variation (%)	105.1	105.1	
Particulate Concentration*			
Wet Catch, GR/DSCF	0.048	0.038	0.043
Dry Catch, GR/DSCF	0.060	0.056	0.058
Total, GR/DSCF	0.108	0.094	0.101
Particulate Emission Rate*			
Total, LB/HR	47.24	41.15	44.20
		wet	18.82
		dry	25.38

*Dry catch plus organic and inorganic/residual wet catch

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TABLE 10
RESULTS OF PARTICULATE LOADING DETERMINATIONS

Parameter	Line No. 1 Dryers	
	Core Dryer	Surface Dryer
Date of Run	6/16/94	6/16/94
Time of Run	1135-1327	735-836
Sample Duration (Min.)	54.0	60.0
Average Flue Gas Temperature (°F)	245.9	247.4
Moisture Content of Flue Gas (%v/v)	21.76	29.74
Particulate Collected (Mg)*		
Wet Catch	87.1	156.3
Dry Catch	266.0	520.9
Total	353.1	677.2
Volumetric Flow Rate		
ACFM	46220	49300
SCFM	32380	34400
DSCFM	25340	24170
Sample Volume (Cubic Feet)		
Meter Conditions	29.65	36.66
Dry Standard	27.08	34.70
Isokinetic Variation (%)	89.1	107.7
Particulate Concentration*		
Wet Catch, GR/DSCF	0.050	0.070
Dry Catch, GR/DSCF	0.152	0.232
Total, GR/DSCF	0.201	0.301
Particulate Emission Rate*		
Total, LB/HR	43.69	62.40
	B ¹ / ₂ 10.87	14.51
	F ¹ / ₂ 32.82	47.89

*Dry catch plus organic/residual wet catch

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TABLE 11
RESULTS OF PARTICULATE LOADING DETERMINATIONS

Line No. 2 EFB Outlet

Parameter	Run 1	Run 1	
Date of Run	6/16/94	6/16/94	
Time of Run	1537-1637	1739-1818	
Sample Duration (Min.)	60.0	39.0	
Average Flue Gas Temperature (°F)	220.8	222.0	
Moisture Content of Flue Gas (%v/v)	22.55	21.70	
Particulate Collected (Mg)*			
Wet Catch	82.3	60.2	
Dry Catch	139.6	73.8	
Total	221.9	134.0	
Volumetric Flow Rate			
ACFM	102570	105800	104185
SCFM	75150	77370	
DSCFM	58200	60590	59395
Sample Volume (Cubic Feet)			
Meter Conditions	50.34	33.76	
Dry Standard	45.92	30.92	
Isokinetic Variation (%)	98.1	97.6	
Particulate Concentration*			
Wet Catch, GR/DSCF	0.028	0.030	0.029
Dry Catch, GR/DSCF	0.047	0.037	0.042
Total, GR/DSCF	0.075	0.067	0.071
Particulate Emission Rate*			
Total, LB/HR	37.20	34.73	35.97 TSP 21.28 F ¹ / ₂ 14.69 B ¹ / ₂

*Dry catch plus organic and inorganic/residual wet catch

Louisiana - Pacific Corporation
 Hayward, Wisconsin
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TABLE 12
RESULTS OF PARTICULATE LOADING DETERMINATIONS

Line No. 2 Dryers

Parameter	Core Dryer Outlet	Surface Outlet
Date of Run	6/16/94	6/16/94
Time of Run	1537-1638	1737-1814
Sample Duration (Min.)	60.0	36.0
Average Flue Gas Temperature (°F)	219.6	217.7
Moisture Content of Flue Gas (%v/v)	18.24	22.50
Particulate Collected (Mg)*		
Wet Catch	154.6	112.3
Dry Catch	473.3	289.2
Total	627.9	401.5
Volumetric Flow Rate		
ACFM	50530	56000
SCFM	36020	40230
DSCFM	29450	31180
Sample Volume (Cubic Feet)		
Meter Conditions	43.15	28.89
Dry Standard	39.03	26.10
Isokinetic Variation (%)	96.3	101.4
Particulate Concentration*		
Wet Catch, GR/DSCF	0.061	0.066
Dry Catch, GR/DSCF	0.187	0.171
Total, GR/DSCF	0.248	0.237
Particulate Emission Rate*		
Total, LB/HR	62.67	63.44
	B ^{1/2} 15.91	17.67
	F ^{1/2} 47.26	45.77

*Dry catch plus organic and inorganic/residual wet catch

RESULTS OF PRELIMINARY SOURCE DETERMINATIONS

TABLE 13
RESULTS OF AIR FLOW DETERMINATIONS

Line No. 1

<u>Parameter</u>	<u>Surface Dryer Outlet</u> 6/15/94	<u>Core Dryer Outlet</u> 6/15/94	<u>EFB Outlet</u> 6/15/94
Date of Run			
Time of Measurement	1530	1111	1244
Number of Sampling Ports	1	2	1
Number of Points Sampled	10	20	12
Barometric Pressure (In. Hg)	28.63	28.63	28.63
Static Pressure (In. WC)	-9.10	-8.10	6.00
Absolute Flue Gas Pressure (In. Hg)	27.96	28.03	29.07
Average Flue Gas Temperature (F)	232	245	235
Average Moisture Content (%v/v)	30.0	21.1	23.3
Dry Molecular Wt. of Gas (lb/lb-mole)	29.3	29.3	29.3
Flue Gas Average Velocity (FPS)	89.40	78.43	66.08
Duct Dimension (Inches)	42.0	42.0	65.3
Duct Cross-sectional Area (Sq. Ft.)	9.62	9.62	23.22
Volumetric Flow Rate			
ACFM	51,600	45,270	92,060
SCFM	36,790	31,770	67,950
DSCFM	25,770	25,060	52,110

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TABLE 14
RESULTS OF AIR FLOW DETERMINATIONS

	Line No. 2	
	Surface Dryer Outlet	EFB Outlet
Date of Run	6/16/94	6/16/94
Time of Measurement	1445	1520
Number of Sampling Ports	2	1
Number of Points Sampled	12	12
Barometric Pressure (In. Hg)	28.63	28.63
Static Pressure (In. WC)	-16.00	6
Absolute Flue Gas Pressure (In. Hg)	27.45	29.07
Average Flue Gas Temperature (F)	220	225
Average Moisture Content (%v/v)	24	25
Flue Gas Average Velocity (Feet/Second)	88.37	71.36
Duct Dimension (Inches)	41.75	65.25
Duct Cross-sectional Area (Square Feet)	9.51	23.22
Volumetric Flow Rate		
ACFM	50410	99420
SCFM	35910	74460
DSCFM	27300	55840

TEST PROCEDURES SUMMARY

Testing on the Line 1 EFB outlet was performed from 2 test ports oriented at 90 degrees, approximately 3.0 duct diameters downstream of the nearest flow disturbance and 1.1 duct diameters upstream of the RTO. The duct dimension at this point was verified on-site and measures 65.25 inches in diameter. A 24 point traverse was used to extract representative flue gas samples. Each point was sampled 2.5 minutes for a run duration of 60 minutes. Test port and traverse point locations are displayed in Figures 1 and 3.

Testing on the Line 1 Core dryer outlet and Surface dryer outlet was performed from 2 test ports oriented at 90 degrees, approximately 5.0 duct diameters downstream of the nearest flow disturbance and 5.7 duct diameters upstream of the EFB. The duct dimension at this point was verified on-site and measures 42.0 inches in diameter. A 20 point traverse was used to extract representative flue gas samples. Each point was sampled 3.0 minutes for a run duration of 60 minutes. Test port and traverse point locations are displayed in Figures 1 and 4.

Testing on the Line 2 EFB outlet was performed from 1 test ports situated on the top of the duct, approximately 4.5 duct diameters downstream of the nearest flow disturbance and 2.9 duct diameters upstream of the RTO. The duct dimension at this point was verified on-site and measures 65.25 inches in diameter. A 12 point traverse was used to extract representative flue gas samples. Each point was sampled 5.0 minutes for a run duration of 60 minutes. Test port and traverse point locations are displayed in Figures 2 and 3.

Testing on the Line 2 Core dryer outlet and Surface dryer outlet was performed from 2 test ports oriented at 90 degrees, approximately 7.2 duct diameters downstream of the nearest flow disturbance and 3.2 duct diameters upstream of the EFB. The duct dimension at this point was verified on-site and measures 41.75 inches in diameter. A 12 point traverse was used to extract representative flue gas samples. Each point was sampled 5.0 minutes for a run duration of 60 minutes. Test port and traverse point locations are displayed in Figures 2 and 5.

TEST PROCEDURES SUMMARY (continued)

Testing on the Line 2 Surface dryer outlet was performed from 2 test ports oriented at 90 degrees, approximately 5.2 duct diameters downstream of the nearest flow disturbance and 3.5 duct diameters upstream of the EFB. The duct dimension at this point was verified on-site and measures 41.75 inches in diameter. A 20 point traverse was used to extract representative flue gas samples. Each point was sampled 3.0 minutes for a run duration of 36 minutes. Test port and traverse point locations are displayed in Figures 2 and 6.

Particulate testing was performed in accordance with EPA Methods 1 - 5, 40 CFR 60, Appendix A. A preliminary velocity traverse and moisture estimation were conducted so that an appropriate sampling nozzle required for isokinetic sample withdrawal could be selected. A PACE sampling train that meets or exceeds the specifications outlined in the above reference was used to collect particulate samples. A temperature controlled glass-lined sampling probe was used to extract flue gas samples and transport them to an all glass filter and cyclone assembly in a temperature controlled oven. The back half of the particulate sampling train consisted of a series of three glass impingers, each of the first two prepared with 100 mls of deionized water, followed by a desiccant packed drying column. In addition, integrated gas samples were collected concurrently with the three particulate runs so that gas composition (Orsat) could be determined. Gas samples were verified in the field with a portable oxygen analyzer to ensure that no leakage occurred between the site and the laboratory. The portable oxygen analyzer was also used to monitor the oxygen content of the flue gas throughout the test.

Air flow determinations were performed in accordance with EPA Method 2 using traverse point protocols specified by EPA Method 1, 40 CFR 60, Appendix A. Point velocity measurements were conducted using a S-Type pitot tube and a Neotronics Model EDM-1 Electronic Digital Manometer. Source gas moisture content was estimated using wet bulb/dry bulb temperature measurements.

Louisiana Pacific Corporation
Hayward, Wisconsin
Line No. 1 Dryers & EFB Outlet

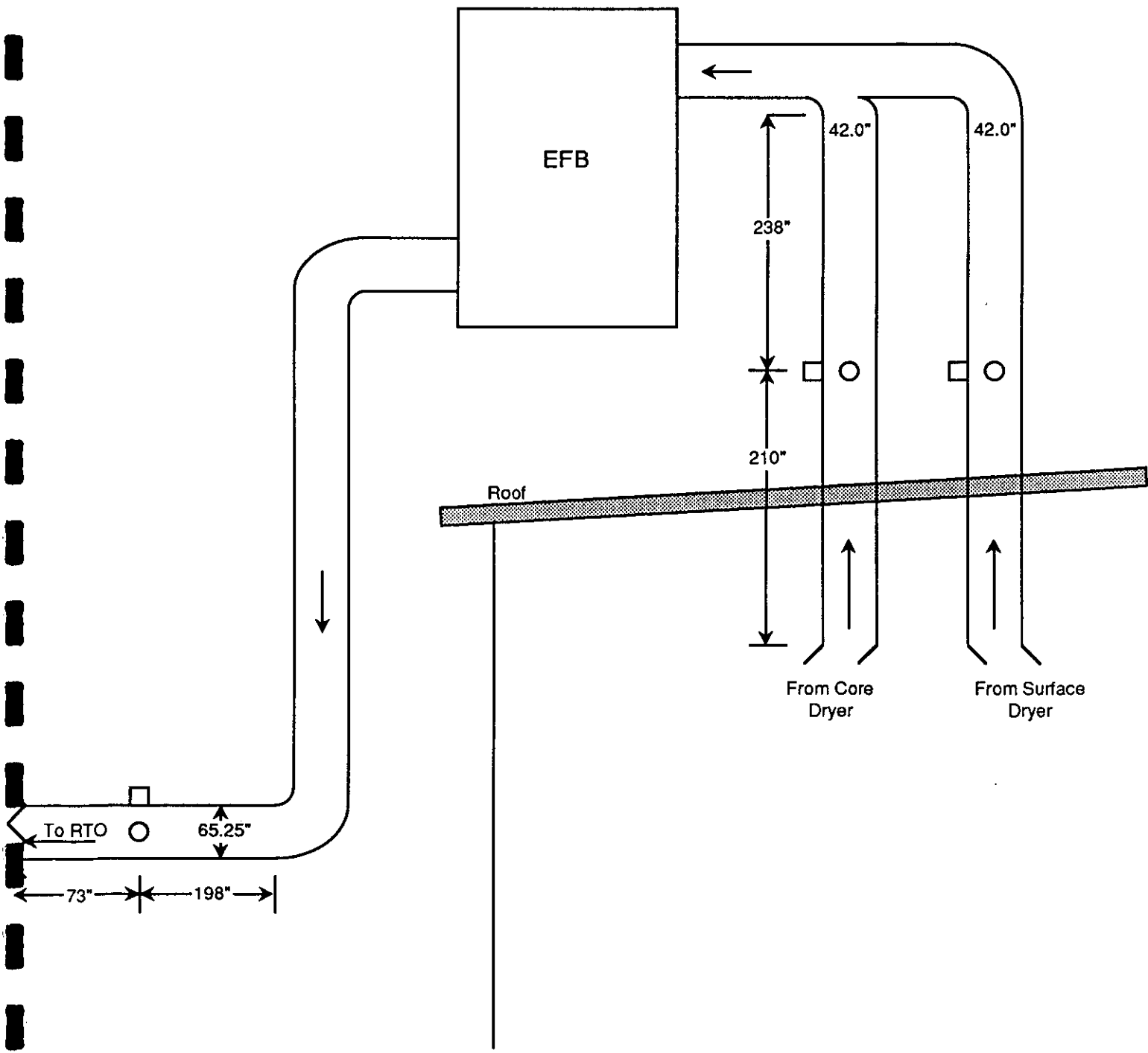


Figure 1
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Louisiana Pacific Corporation
Hayward, Wisconsin
Line No. 2 Dryers & EFB Outlet

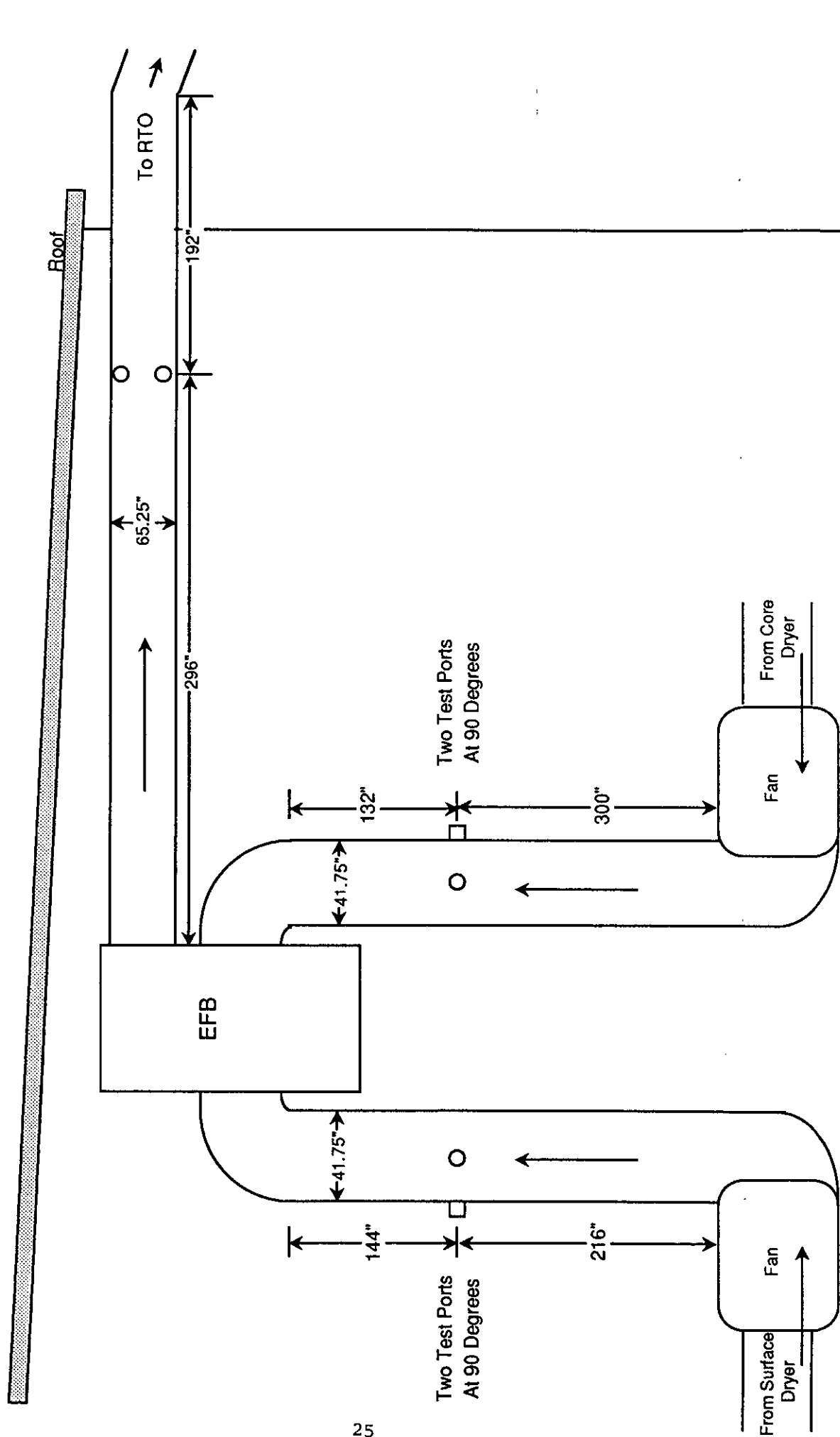
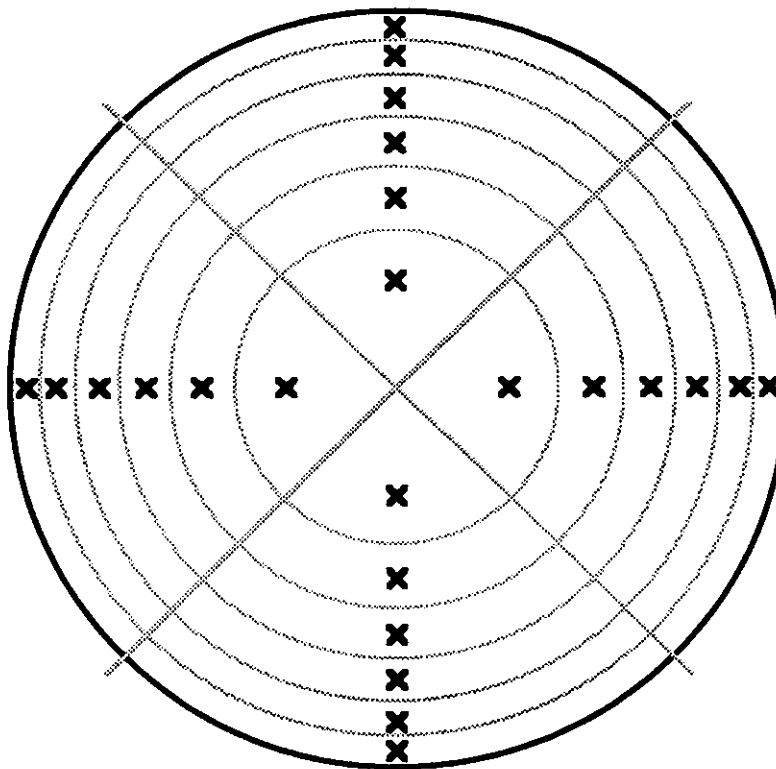


Figure 2

Louisiana-Pacific Corporation

Hayward, Wisconsin
Line No. 1 and Line No. 2
EFB Outlets

Location of Traverse Points



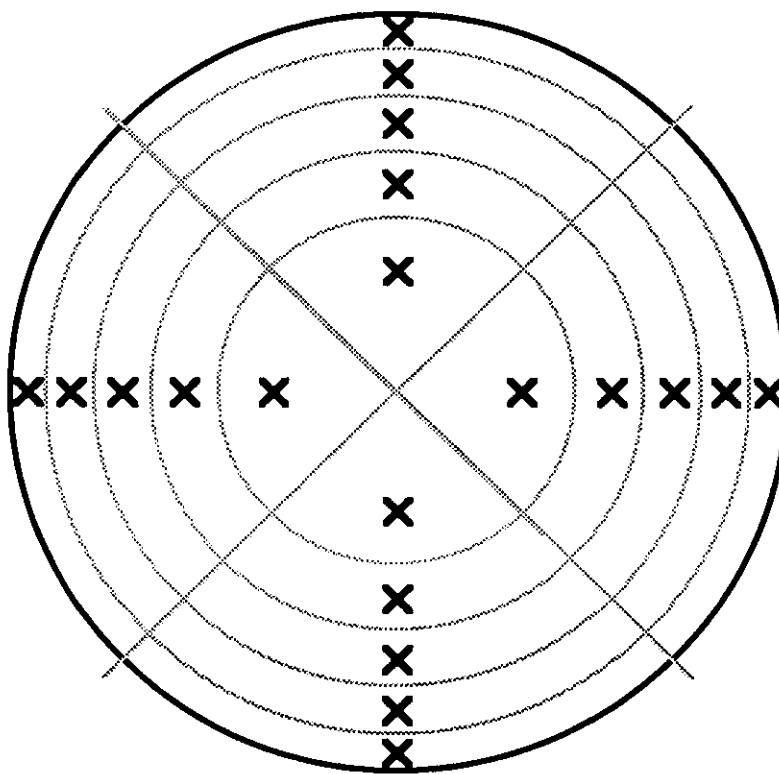
Number of Test Ports	2
Total Number of Traverse Points	24*
Number of Traverse Points Per Traverse	12
Duct Diameter (Inches)	65.25

* The No. 2 Line utilized only 1 port with 12 points.

Louisiana-Pacific Corporation

Hayward, Wisconsin
Line No. 1 Core Dryer and
Surface Dryer Outlets

Location of Traverse Points



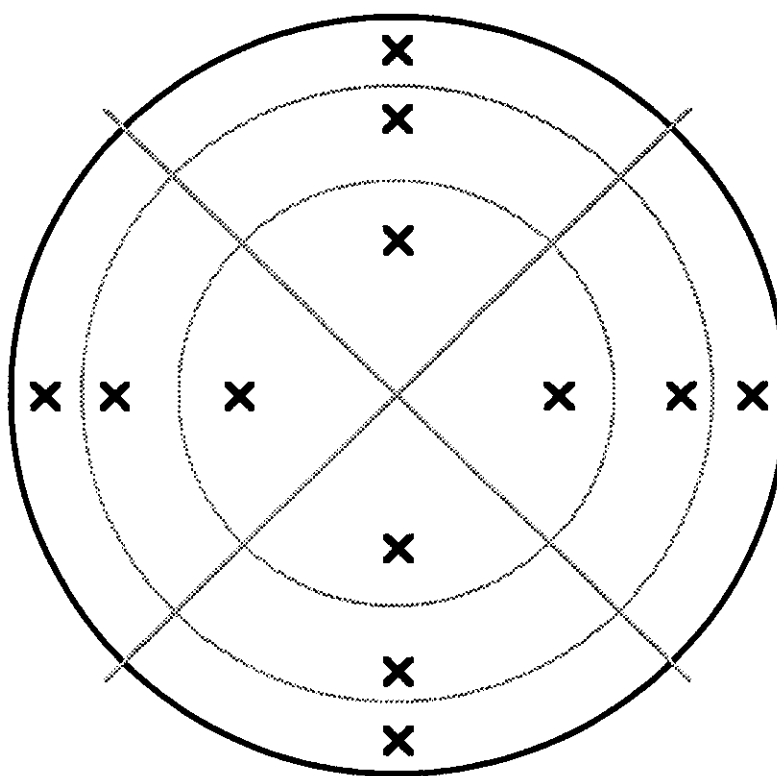
Number of Test Ports	2
Total Number of Traverse Points	20
Number of Traverse Points Per Traverse	10
Duct Diameter (Inches)	42.0

Figure 4
27

Louisiana-Pacific Corporation

Hayward, Wisconsin
Line No. 2 Core Dryer Outlet

Location of Traverse Points

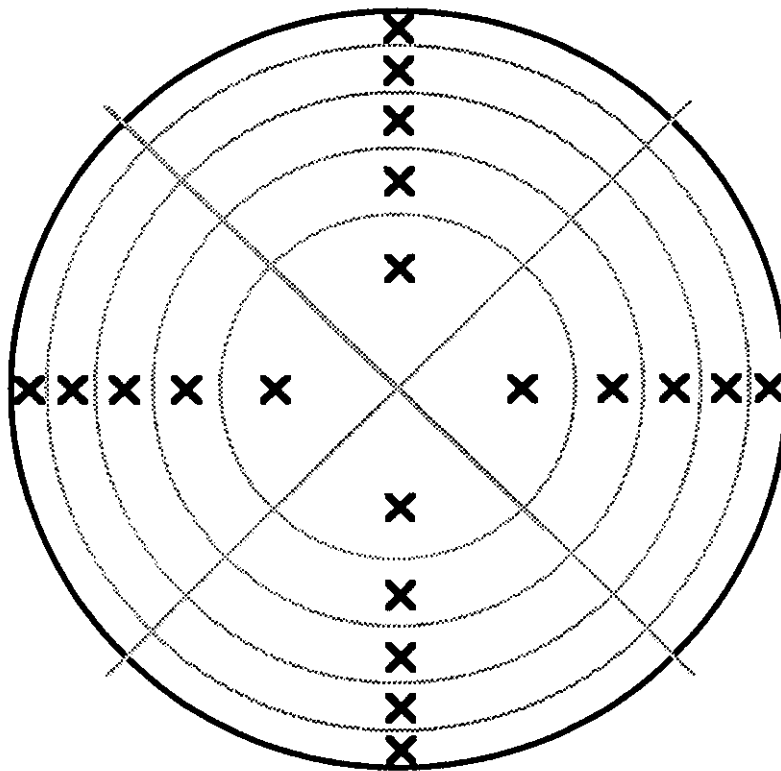


Number of Test Ports	2
Total Number of Traverse Points	12
Number of Traverse Points Per Traverse	6
Duct Diameter (Inches)	41.75

Louisiana-Pacific Corporation

Hayward, Wisconsin
Line No. 2 Surface Dryer Outlet

Location of Traverse Points



Number of Test Ports	2
Total Number of Traverse Points	20
Number of Traverse Points Per Traverse	10
Duct Diameter (Inches)	41.75

Figure 6
29

APPENDIX A
Field Data Sheets and Notes

EPA METHODS 2-5 FIELD DATA SHEETS

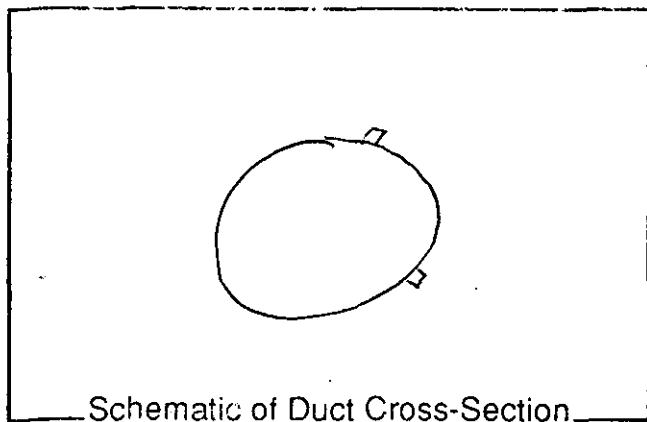
EPA Method 2 Field Data Sheet

Project L.P. Hayward
Test Location EFB Outlet
Date 6/15/94 Test 1 Run _____
Operators JEP MEW
Barometric Pressure 28.55 Inches Hg
Static Pressure 6.0 Inches H₂O
Pitot Leak Check - Positive _____ Negative _____

Pitot Tube No. 8 C_p .842
Pressure Measurement Device Oil Manometer
Duct Dimensions 65.25 Inches
Port Length 6.25 Inches
Temp. - Dry Bulb 235 °F, Wet Bulb 150 °F
Moisture Content 22 %
320P Oxygen Concentration 19 %
Time of Measurement 1244 (24 Hr. Clock)

Traverse Point Identification				Cyclonic Flow Yaw Angle	Velocity Head ΔP Inches H ₂ O	Stack Temperature ° F
Point Number	% Of Diameter	Inches From:				
		Wall	Port			
A 1		6.39	7.64	°	.80	
2		4.37	10.62	°	.86	
3		7.71	13.96	°	1.65	
4		11.57	17.82	°	1.00	
5		16.31	22.56	°	1.60	
6		23.21	29.46	°	.94	
7		42.04	48.29	°	.89	
8		48.94	55.19	°	.88	
9		53.68	59.93	°	.87	
10		57.54	63.79	°	1.02	
11		60.88	67.13	°	1.10	
12		63.86	70.11	°	.95	
B 1				°	.	
2				°	.	
3				°	.	
4				°	.	
5				°	.	
6				°	.	
7				°	.	
8				°	.	
9				°	.	
10				°	.	
11				°	.	
12				°	.	

AC
ΔP
.947
227
1/4"



Computer Data Summary:

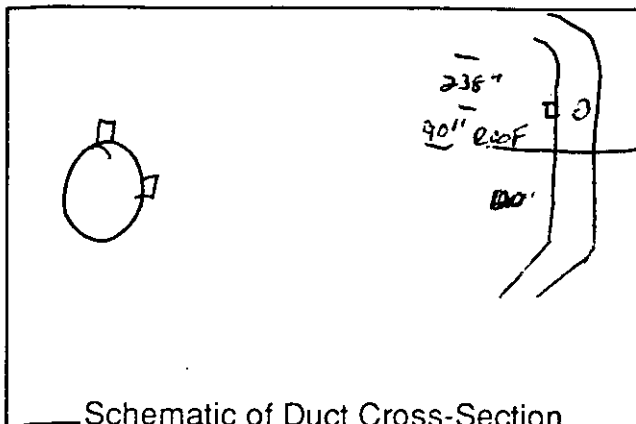
Stack Pressure _____ Inches Hg
Duct Area _____ Square Feet
Molecular Weight - M_d _____
Molecular Weight - M_s _____
Avg. Duct Temperature _____ ° F
Average √ΔP _____
Flue Gas Velocity _____ Feet/Sec.
Volumetric Flow Rate:
ACFM _____
DSCFM _____

EPA Method 2 Field Data Sheet
Multiple Determinations

Project LP HAYWARD
Test Location Line 1 ~~core dryer~~
Date 6-15-84 Test 1 Run
Operators MSL KSL
Pitot Tube No. 2 C_p .535
Duct Dimensions 42.0 Inches
Port Length 8.0 Inches
Pitot Leak Check - Positive OK Negative OK

	Run 1	Run 2	Run 3	Run 4
Bar. Press.-In. Hg	28.53 →		28.53	
Stat. Press.- In.WC	-8.1 →		-9.1	
Temp.-Dry Bulb-°F	24.5 →		23.2	
Temp.-Wet Bulb-°F	14.6 →		15.7	
Moist. Content-%	21 →		22.3	
320P Oxygen-%	19 →		17	
Time of Meas.	1111 →		1530	

Traverse Point I.D.			Cyclonic Flow Yaw $\angle$	Velocity Head - Inches H ₂ O				Stack Temperature - ° F			
Point No.	Inches From:			Run 1 Δ P	Run 2 Δ P	Run 3 Δ P	Run 4 Δ P	Run 1 Temp.	Run 2 Temp.	Run 3 Temp.	Run 4 Temp.
	Wall	Port									
A 1	1.08	9.08		1.05	.85	1.05					
2	3.43	11.43		1.05	1.10	1.50					
3	6.15	14.15		1.10	1.10	1.60					
4	9.50	17.50		1.10	1.10	1.55					
5	14.36	22.36		1.15	1.10	1.55					
6	27.64	35.64		1.25	1.25	1.55					
7	32.50	40.50		1.45	1.40	1.80					
8	35.85	43.85		1.55	1.50	2.00					
9	38.57	46.57		1.60	1.60	2.20					
10	40.92	48.92		1.65	1.60	2.15					
B 1				1.00	.85						
2				1.20	1.30						
3				1.35	1.30						
4				1.30	1.30						
5				1.35	1.30						
6				1.30	1.30						
7				1.50	1.40						
8				1.55	1.50						
9				1.65	1.60						
10				1.65	1.60						
					1.30						
					.216						
					3/16						



Computer Data Summary: <u>surface dryer</u>				
PC-6 Output	Run 1	Run 2	Run 3	Run 4
Stack Pres. - In. Hg				
Duct Area - Sq. Ft.				
Mole. Weight - M_d				
Mole. Weight - M_s				
Avg. Temp. - °F				
Average $\sqrt{\Delta P}$				
Gas Vel. - Ft./Sec.				
ACFM				
DSCFM				

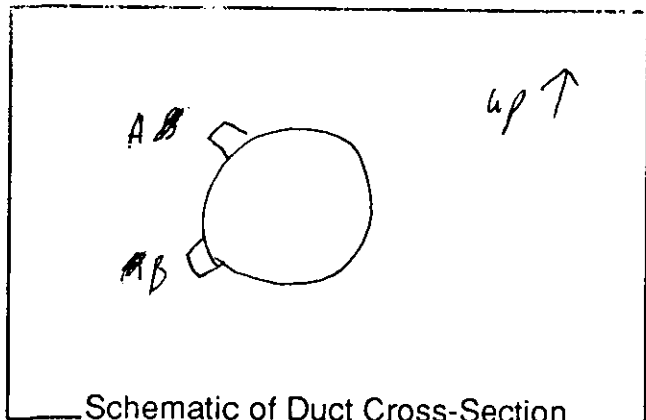
EPA Method 2 Field Data Sheet

Project L. P. Hayward
 Test Location Line 2 EFB Outlet
 Date 6-16-94 Test 1 Run
 Operators JEP MEW
 Barometric Pressure 28.63 Inches Hg
 Static Pressure -5 Inches H₂O
 Pitot Leak Check - Positive OK Negative OK

Pitot Tube No. 24 C_p 843
 Pressure Measurement Device 0.1 Maxnote
 Duct Dimensions 60.65.25 Inches
 Port Length 14.75 Inches
 Temp. - Dry Bulb 225 °F, Wet Bulb 148 °F
 Moisture Content 25 %
 320P Oxygen Concentration 17 %
 Time of Measurement 1520 (24 Hr. Clock)

Traverse Point Identification				Cyclonic Flow Yaw Angle	Velocity Head ΔP Inches H ₂ O	Stack Temperature ° F
Point Number	% Of Diameter	Inches From:				
		Wall	Port			
A 12		1.39	7.39/16.14	°	.95	
11		4.37	10.37/19.12	°	.86	
10		7.71	13.71/22.46	°	1.02	
9		11.57	17.57/26.32	°	1.10	
8		16.31	22.31/31.06	°	1.15	
7		23.21	29.21/37.96	°	1.20	
6		42.04	48.04/56.74	°	1.05	
5		48.94	54.94/63.69	°	1.05	
4		53.64	59.64/68.43	°	1.20	
3		57.54	63.54/72.29	°	1.20	
2		60.88	66.88/75.63	°	1.25	
1		63.86	69.86/78.61	°	1.85	
B 12				°	.	
11				°	.	
10				°	.	
9				°	.	
8				°	.	
7				°	.	
6				°	.	
5				°	.	
4				°	.	
3				°	.	
2				°	.	
1				°	.	

Avg
1.00
1.224
1/4



Computer Data Summary:

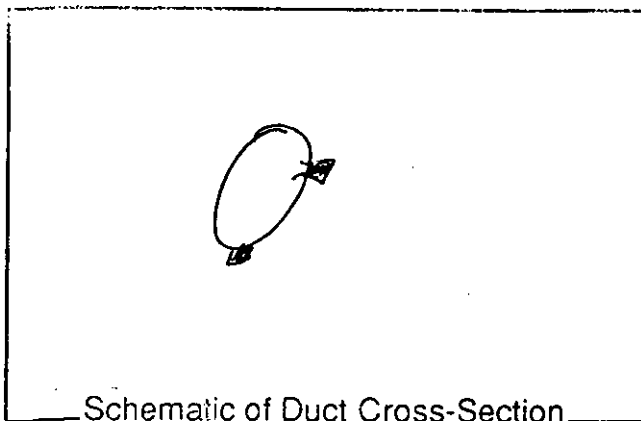
Stack Pressure _____ Inches Hg
 Duct Area _____ Square Feet
 Molecular Weight - M_d _____
 Molecular Weight - M_s _____
 Avg. Duct Temperature _____ ° F
 Average √ΔP _____
 Flue Gas Velocity _____ Feet/Sec.
 Volumetric Flow Rate:
 ACFM _____
 DSCFM _____

EPA Method 2 Field Data Sheet

Project LP HAYWARD
Test Location Line 2 core dryer out
Date 6-16-94 Test 1 Run _____
Operators MSL KSL
Barometric Pressure 28.63 Inches Hg
Static Pressure -16.8 core Inches H₂O
Pitot Leak Check - Positive OK Negative OK

Pitot Tube No. 2 C_p 835
Pressure Measurement Device 0.2 mmHg
Duct Dimensions 41.75 Inches
Port Length 4.25 Inches
Temp. - Dry Bulb 220 °F, Wet Bulb 150 °F
Moisture Content 24 %
320P Oxygen Concentration 17 %
Time of Measurement 1445 (24 Hr. Clock)

Traverse Point Identification				Cyclonic Flow Yaw Angle	Velocity Head ΔP Inches H ₂ O	Stack Temperature °F
Point Number	% Of Diameter	Inches From:				
		Wall	Port			
A	1	1.82	6.07	°	1.40	
	2	6.11	10.36	°	2.05	
	3	12.35	16.60	°	1.70	
	4	29.40	33.65	°	1.40	
	5	35.64	39.89	°	1.70	
	6	39.93	44.18	°	1.80	
B	1			°	.98	
	2			°	1.25	1.67
	3			°	1.30	203
	4			°	1.80	316
	5			°	2.20	
	6			°	2.40	
A	1	1.07	5.32	°	.	
	2	3.41	7.66	°	.	
	3	6.11	10.36	°	.	
	4	9.44	13.69	°	.	
	5	14.27	18.52	°	.	
	6	27.48	31.73	°	.	
B	7	32.31	36.56	°	.	
	8	35.64	39.89	°	.	
	9	38.34	42.59	°	.	
	10	40.68	44.93	°	.	
				°	.	
				°	.	



Computer Data Summary:

Stack Pressure _____ Inches Hg
Duct Area _____ Square Feet
Molecular Weight - M_d _____
Molecular Weight - M_s _____
Avg. Duct Temperature _____ °F
Average √ΔP _____
Flue Gas Velocity _____ Feet/Sec.
Volumetric Flow Rate:
ACFM _____
DSCFM _____

Field Computer Summary

Project Name: L.P. Hayward
Sampling Location: EFB Outlet
Date of Test: 6/15/94
Test Number: 1

Operator JEP

Initialization Parameters	Run Specific Input Parameters			
	Core	Surface	Surface	Core
	Test 1	Test 2	Test 2	Test 1
	Run 1	Run 2	Run 2	Run 2
Change meter before run 1,0044				
Meter Coef. - ∂ = 1.0067	VIO 203.60	226.40	253.60	298.00
Orif. Coef. - $\Delta H @$ = 2.039	No. Of Points 24	24	24	12
Pitot Coef. - C_p = 1.842	MC 22		24	25
Nozzle Dia. - D_n = .234	VIF 225.37	253.15	297.76	343.12
Bar. Pres. - P_b = 28.55/28.63	Grams H_2O 108	175	306	323
Time/Point - ΔT = 2.5	Run Time 30	33.5	60	60
Moisture Content = 22	1-Rnd/2-Rect 65.25	65.25	65.25	65.25
% Oxygen = 19	Diameter(Ins.)			
Meter Temp. - t_m = 90	Length(Ins.)			
Static Pres. - P_g = 6	Width(Ins.)			

End Of Run Summary

	Run 1	Run 2	Run 3	Run 4
Avg. ΔP	0.994	0.997	0.974	0.989
Avg. ΔH	1.693	1.671	1.514	1.546
Avg. t_s	238.50	239.42	234.83	242.00
Avg. t_m	96.63	86.00	78.96	92.08
Standard Vol.	19.88	24.90	41.74	41.64
Moist. Content	20.37	24.86	25.65	26.75
Avg. Gas Vel.	69.14	69.34	67.70	69.21
% Isokinetic	96.71	107.66	103.35	103.40
ACFM	96329	94613	94316	96425
DSCFM	54476	51484	50201	50052

EPA Method 5 Field Data Sheet

Project L.P. Hayward Train No. 84 CM-7 P2 Pitot Tube No. 24 C_p .843 Sampling Train Leak Checks:
Sample Location EFB Outfall Meter Coef. 0.10044 Bar. Pres. 28.63 Ins. Hg Pretest 0.00 @ 15 Ins. Hg
Date 6-16-94 Test 2 Run 2 Orifice Coef. ΔH@16.85 Static Pres. 6 Ins. H₂O Posttest 0.00 @ 15 Ins. Hg
Operators JEP MEW Nozzle No. 7-2 D_n 235 Estimated MC 24 % Pitot - Positive 0.0 Negative 0.0

Point No.	Time ΔT	Meter Vol. V _m Cubic Feet	Velocity Head - ΔP Inches WC	Orifice Meter - ΔH Inches WC	Desired ΔV _m	Desired V _m	Vacuum Inches Hg	Stack Temp. ° F	Sampling Train Temperatures - ° F					320 P Oxygen Percent
									Filter	Probe	Impinger Outlet	Meter Inlet	Meter Outlet	
A 12	(0737) 5	257.19	.40	1.44	360	720	3.9	233			59	71	73	17.1
11	16	260.65	.88	1.39	351	471	4.5	233			57	71	75	18.1
10	15	264.07	.85	1.35	346	417	5.0	232			55	71	71	18.1
9	20	267.55	.86	1.32	349	765	5.3	232			56	81	72	17.5
8	25	271.28	.94	1.50	366	132	5.8	230			56	83	72	15.1
7	30	275.01	.98	1.57	375	506	6.1	231			56	84	73	15.2
6	35	278.84	1.05	1.68	388	894	8.5	237			57	86	74	15.5
5	40	282.72	1.05	1.66	387	281	8.5	241			56	87	75	14.9
4	45	286.67	1.05	1.67	388	669	8.3	240			58	88	76	15.3
3	50	290.33	.92	1.47	364	433	8.0	238			58	89	77	15.6
2	55	294.12	.97	1.55	375	407	8.0	238			59	90	79	16.2
1	60	297.76	.95	1.53	372	779	8.4	237			59	91	79	14.8
	(0837)													

Samples Recovered: Filter No. 31 #10 ; ☒ Probe Wash; ☒ Wet Catch; ☐ Other _____

Integrated Gas Sampling Data:

Box No. 84 Bag Material Tedlar
Bag No. 1 Leak Checks 0.00 cc/min. @ 25" Hg
Bag Vol. 40 Liters Posttest O₂ Reading 0X-1
320 P No. 0X-1

Moisture Recovery Data:

1	2	3	4	Desiccant	Total
360	138	3		1435	
100	100	0		1430	
260	38	3		3	306



A [REDACTED] SAMP [REDACTED] IN [REDACTED] P [REDACTED] ME

Project L. P. Hayward Train No. 04 CH-782 Pitot Tube No. 24 C₀ 1843

Sample Location Live / (Live Pres) / Ebb / Ditch Meter Coef. @ 1.0044 Bar. Pres. 28.63 Ins. Hg. _____
 Date 1-11-94 Test 1 Date _____ Coef. @ _____

Office Coel. $\Delta H @ 1100^\circ F$	Static Pres.	Ins. H_2O
Nozzle No 3-2	Estimated MC	%
Operators JEP		
Date 2-26-77	Test 1	Run 2

	Mater Val	Vale-ble	Crit-	Val-	Estimated MC	%
NOZZLE NO.					27	

Pretest 4.00 / @ 15 Ins. HgPosttest 0.001 @ 15 Ins. Hg

FLU1 - Positive	FLU1 - Negative
1	1
2	2
3	3
4	4
5	5
6	6
7	7
8	8
9	9
10	10
11	11
12	12
13	13
14	14
15	15
16	16
17	17
18	18
19	19
20	20
21	21
22	22
23	23
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73	73
74	74
75	75
76	76
77	77
78	78
79	79
80	80
81	81
82	82
83	83
84	84
85	85
86	86
87	87
88	88
89	89
90	90
91	91
92	92
93	93
94	94
95	95
96	96
97	97
98	98
99	99
100	100

Samples Recovered: Filter No. 3m #5 thistle ☒ Probe Wash; ☒ Wet Catch; ☐ Other _____

Moisture Recover Data:

Bag Material Tedlar

Leak Checks 6.66 cc/min. @ 25"Hg
Positive Pressure Reading

320 P No. 11X-1

Impinger No.	1	2	3	4	Desiccant	Total
Final Volume	326	177	3		1476	
Initial Volume	166	166	6		1419	
Difference	160	11	3		17	57

Field Computer Summary

Project Name: LP Hayward
Sampling Location: core dryer line 1 outlet
Date of Test: 6-15-94
Test Number: 1

Operator M. Loffus

Initialization Parameters	Run Specific Input Parameters			
	core dryer Line 1	surface dryer Line 1	surface dryer Line 2	core dryer Line 1
	Run 1	Run 2	Run 2	Run 2
Meter Coef. - α = <u>.9992</u>	V/O <u>321.89</u>	<u>346.70</u>	<u>370.00</u>	<u>407.00</u>
Orif. Coef. - $\Delta H @$ = <u>1.760</u>	No. Of Points <u>20</u>	<u>20</u>	<u>20</u>	<u>20</u>
Pitot Coef. - C_p = <u>.835</u>	MC <u>21</u>	<u>26</u>	<u>24</u>	<u>28</u>
Nozzle Dia. - D_n = <u>.198</u>	V/F <u>344.20</u>	<u>369.85</u>	<u>406.66</u>	<u>436.65</u>
Bar. Pres. - P_b = <u>28.55</u>	Grams H ₂ O <u>165</u>	<u>187</u>	<u>312</u>	<u>160</u>
Time/Point - ΔT = <u>3</u>	Run Time <u>30.0</u>	<u>37.460</u>	<u>60</u>	<u>52</u>
Moisture Content = <u>21</u>	1-Rnd/2-Rect <u>1</u>	<u>1</u>	<u>1</u>	<u>1</u>
% Oxygen = <u>19</u>	Diameter(Ins.) <u>42</u>	<u>42</u>	<u>42</u>	<u>42</u>
Meter Temp. - t_m = <u>72</u>	Length(Ins.) <u>X</u>	<u>X</u>	<u>X</u>	<u>X</u>
Static Pres. - P_g = <u>-8.1</u>	Width(Ins.) <u>X</u>	<u>X</u>	<u>X</u>	<u>X</u>

surface
6/16

core

.9992
1.760
.835

28.63

3

24

17

70

-9.0.

-8.2

End Of Run Summary

	Run 1	Run 2	Run 3	Run 4
Avg. $\sqrt{\Delta P}$	<u>1.167</u>	<u>1.234</u>	<u>1.214</u>	<u>1.158</u>
Avg. ΔH	<u>1.071</u>	<u>1.090</u>	<u>1.091</u>	<u>1.052</u>
Avg. t_s	<u>246.58</u>	<u>247.15</u>	<u>247.35</u>	<u>240.50</u>
Avg. t_m	<u>93.96</u>	<u>81.23</u>	<u>71.30</u>	<u>94.03</u>
Standard Vol.	<u>20.33</u>	<u>21.59</u>	<u>349.3</u>	<u>2708</u>
Moist. Content	<u>27.64</u>	<u>28.96</u>	<u>28.60</u>	<u>21.76</u>
Avg. Gas Vel.	<u>86.50</u>	<u>86.78</u>	<u>84.51</u>	<u>80.81</u>
% Isokinetic	<u>106.98</u>	<u>103.87</u>	<u>109.38</u>	<u>91.00</u>
ACFM	<u>47048</u>	<u>50095</u>	<u>48782</u>	<u>46647</u>
DSCFM	<u>23767</u>	<u>24826</u>	<u>23963</u>	<u>25769</u>

EPA Method 5 Field Data Sheet

Project CP Hayward Surface Train No. CS 62 P1 Pitot Tube No. 2 C_p 835 Sampling Train Leak Checks:
 Sample Location Line 1 Meter Coef. 0.9992 Bar. Pres. 28.63 Ins. Hg Pretest 0.02 @ 15 Ins. Hg
 Date 6-16-84 Test 2 Run 2 Orifice Coef. ΔH@1760 Static Pres. ~2.0 Ins. H₂O Posttest 0.00 @ 6.1 Ins. Hg
 Operators msc Kik Nozzle No. 4-1 D_n 198 Estimated MC 24 % Pitot - Positive OK Negative OK

Point No.	Time ΔT	Meter Vol. V _m Cubic Feet	Velocity Head - ΔP Inches WC	Orifice Meter - ΔH Inches WC	Desired ΔV _m	Desired V _m	Vacuum Inches Hg	Stack Temp. °F	Sampling Train Temperatures - °F					320 P Oxygen Percent
									Filter	Probe	Impinger Outlet	Meter Inlet	Meter Outlet	
A 10	3	373.13	1.90	1.39	208	308	4.2	248	250	250	67	67	69	
9	6	374.13	1.95	1.41	209	417	4.2	253	250	240	50	68	69	
8	9	376.04	1.85	1.34	204	621	4.2	252	251	247	57	72	69	
7	12	378.03	1.65	1.21	194	815	4.5	257	250	249	54	73	69	
6	15	379.95	1.50	1.10	185	999	4.8	262	249	248	54	75	70	
5	18	381.68	1.30	.95	173	172	4.5	250	250	249	60	76	70	
4	21	383.66	1.40	1.03	179	357	5.2	251	249	251	61	76	70	
3	24	385.50	1.40	1.03	179	530	5.2	252	249	252	61	78	71	
2	27	387.33	1.45	1.07	183	713	5.5	247	250	250	61	78	71	
1	30	388.79	.93	.69	147	861	4.1	244	249	249	63	79	73	
B 10	33	390.68	1.85	1.28	194	854	6.5	250	249	253	63	77	73	
9	36	392.66	1.80	1.24	190	245	6.6	250	251	230	61	78	73	
8	39	394.60	1.85	1.36	206	451	6.9	255	253	228	62	80	73	
7	42	396.45	1.70	1.25	199	649	6.9	252	253	237	62	81	74	
6	45	398.30	1.50	1.11	187	834	7.1	253	243	243	63	81	74	
5	48	400.01	1.20	.89	167	803	6.5	252	249	244	64	82	74	
4	51	401.77	1.30	.96	174	177	6.5	253	249	248	65	82	75	
3	54	403.47	1.20	.91	170	347	6.1	233	249	247	65	82	75	
2	57	405.12	1.10	.86	164	511	6.3	218	249	248	65	83	75	
1	60	406.66	.98	.75	154	665	6.2	232	249	241	65	83	76	
	(0836)													

Samples Recovered: Filter No. 3215 ; ☒ Probe Wash; ☒ Wet Catch; ☐ Other Down = 0525

Integrated Gas Sampling Data:

Box No. 2 Bag Material Redlar
 Bag No. 3 Leak Checks 1.00 cc/min. @ 25" Hg
 Bag Vol. 40 Liters Posttest O₂ Reading
 320 P No.

Moisture Recovery Data:

Impinger No.	Final Volume	Initial Volume	Difference
1	348	151	0
2	100	100	0
3	248	51	0
4	137	137	0
5	136	136	0
6	13	13	0
7	312	312	0

154

Field Computer Summary

Project Name: L.P. Hayward
 Sampling Location: Line 2 EFB Outlet
 Date of Test: 6-16-94
 Test Number: _____

Operator JEL

Initialization Parameters	Run Specific Input Parameters			
	Run 1	Run 2	Run 3	Run 4
Meter Coef. - ∂ = <u>1.942</u>	VIO <u>486.50</u>	<u>488.30</u>	<u>523.50</u>	
Orif. Coef. - $\Delta H @$ = <u>1.760</u>	No. Of Points <u>12</u>	<u>12</u>	<u>12</u>	
Pitot Coef. - C_p = <u>.843</u>	MC <u>25</u>	<u>25</u>	<u>25</u>	
Nozzle Dia. - D_n = <u>.239</u>	VIF <u>28487.14</u>	<u>522.06</u>	<u>574.49</u>	
Bar. Pres. - P_b = <u>28.63</u>	Grams H_2O <u>284</u>	<u>182</u>	<u>186</u>	
Time/Point - ΔT = <u>25.5</u>	Run Time <u>60</u>	<u>39</u>	<u>60</u>	
Moisture Content = <u>25</u>	1-Rnd/2-Rect <u>1</u>	<u>1</u>	<u>1</u>	
% Oxygen = <u>17</u>	Diameter(Ins.) <u>65.25</u>	<u>65.25</u>	<u>65.25</u>	
Meter Temp. - t_m = <u>90</u>	Length(Ins.) _____	_____	_____	
Static Pres. - P_g = <u>-5</u>	Width(Ins.) _____	_____	_____	

End Of Run Summary

	Run 1	Run 2	Run 3	Run 4
Avg. $\sqrt{\Delta P}$	<u>1.074</u>	<u>1.110</u>	<u>1.089</u>	<u> </u>
Avg. ΔH	<u>1.963</u>	<u>2.085</u>	<u>2.022</u>	<u> </u>
Avg. t_s	<u>220.75</u>	<u>222.00</u>	<u>210.58</u>	<u> </u>
Avg. t_m	<u>97.46</u>	<u>91.44</u>	<u>84.58</u>	<u> </u>
Standard Vol.	<u>45.92</u>	<u>30.92</u>	<u>47.28</u>	<u> </u>
Moist. Content	<u>22.55</u>	<u>21.70</u>	<u>15.63</u>	<u> </u>
Avg. Gas Vel.	<u>73.26</u>	<u>76.33</u>	<u>74.31</u>	<u> </u>
% Isokinetic	<u>97.85</u>	<u>97.01</u>	<u>90.45</u>	<u> </u>
ACFM	<u>102799</u>	<u>106343</u>	<u>103534</u>	<u> </u>
DSCFM	<u>58333</u>	<u>60895</u>	<u>64971</u>	<u> </u>



EPA Method 5 Field Data Sheet

SAFETY INFORMATION

Project L.P. Hay ward Train No. 14-511 Pitot Tube No. 24 C_p 1.842 Sampling Train Leak Checks:
Sample Location Line 7855 EFB Outlet Meter Coef. 0.9942 Bar. Pres. 28.63 Ins. Hg Pretest 0.001 @ 15 Ins. Hg
Date 6-16-94 Test 1 Run 1 Office Coef. ΔH@1.70 Static Pres. -5 Ins. H₂O Posttest 0.001 @ 11 Ins. Hg
Operators JEP MFW Nozzle No. 3-2 D_n 234 Estimated MC 25 % Pitot - Positive 0.0 Negative 0.0

Point No.	Time ΔT	Meter Vol. V _m Cubic Feet	Velocity Head - ΔP Inches WC	Orifice Meter - ΔH Inches WC	Desired ΔV _m	Desired V _m	Vacuum Inches Hg	Stack Temp. °F	Sampling Train Temperatures - °F					320 P Oxygen Percent
									Filter	Probe	Impinger Outlet	Meter Inlet	Meter Outlet	
A 12	5	441.10	1.36	2.21	445	125	7.5	212			65	90	88	
11	10	445.40	1.20	2.05	426	550	7.4	220			67	91	90	
16	15	449.69	1.20	2.04	427	478	7.6	218			67	93	90	
9	20	453.98	1.20	2.04	428	405	8.5	220			67	95	81	
8	25	458.70	1.15	1.96	420	824	8.6	218			68	96	80	
7	30	462.52	1.20	2.04	428	254	8.9	222			68	94	92	
6	35	466.82	1.20	2.04	428	682	9.2	222			66	97	92	
5	40	471.05	1.20	2.04	429	111	9.2	223			65	97	93	
4	45	475.17	1.10	1.87	411	52	9.0	222			64	97	94	
3	50	479.25	1.10	1.87	411	432	9.2	223			64	97	94	
2	55	483.30	1.05	1.79	402	316	9.0	222			61	97	95	
1	60	487.14	0.95	1.62	383	719	9.0	222			62	96	95	
(1637)														
0-60		V _m = 50.34	1.074	ΔH = 1.963				T _s = 20.75					T _m = 93.46	

Samples Recovered: Filter No. HP11 ; ☒ Probe Wash; ☒ Wet Catch; ☐ Other _____

Integrated Gas Sampling Data:

Box No. 02 Bag Material Teflon
Bag No. 1 Leak Checks 0.00 cc/min. @ 25" Hg
Bag Vol. 46 Liters Posttest O₂ Reading 0.00
320 P No. 014

Moisture Recovery Data:

1	2	3	4	Desiccant	Total
325	130	7		157	
140	140	0		1435	
225	30	7		22	281

Project L. P. Hayward

Project Lin. P. Hayward
 Sample Location Line 2 (Sister) FFB Delta
 Date 6-16-94 Test 2 Run 1
 Operators JEP MFw
 Train No. 62 Cn 5 Yl
 Meter Coef. 0 19942
 Orifice Coef. ΔH@ 1740
 Nozzle No. 3-2 Dn 239
 Pitot Tube No. 24 Cp 1843
 Bar. Pres. 28.63 Ins. Hg
 Static Pres. -5 Ins. H₂O
 Estimated MC 25 %
 Sampling Train Leak Checks:
 Pretest 0.00 @ 15 Ins. Hg
 Posttest 0.00 @ 10 Ins. Hg
 Pitot Positive 0.0 Negative 0.0

[illegible]

Samples Recovered: Filter No. HP-14 ; ☒ Probe Wash; ☒ Wet Catch; ☐ Other _____

Integrated Gas Sampling Data:

Box No. B2 Bag Material Tru Seal
 Bag No. 2 Leak Checks Good cc/min. @ 25"Hg
 Bag Vol. 40 Liters Posttest O₂ Reading
 320 P No. None

Moisture Recovery Data:

Impinger No.	1	2	3	4	Desiccant	Total
Final Volume	186	78	3	X	1472	
Initial Volume	100 50	50	0		7402 1457	
Difference	136	28	3		115	182

EPA Method 5 Field Data Sheet

Project L.P. Hayward
 Sample Location Line 2 FFB 0.1/1
 Date 6-14-94 Test 3 Run 1
 Operators JEP MEK
 Train No. 02 043 04
 Meter Coef. 0.9342
 Orifice Coef. $\Delta H @$ 1.760
 Nozzle No. 3-2 D_n 232
 Pitot Tube No. 24 C_p 0.848
 Bar. Pres. 28.63 Ins. Hg
 Static Pres. -5 Ins. H₂O
 Estimated MC 25 %
 Sampling Train Leak Checks:
 Pretest 0.002 @ 15 Ins. Hg
 Posttest 0.002 @ 2 Ins. Hg
 Pitot Positive 0.0 Negative 0.0

[illegible]

Samples Recovered: Filter No. _____ : ☒ Probe Wash; ☒ Wet Catch; ☐ Other _____

Integrated Gas Sampling Data:

Box No.	<u>B2</u>	Bag Material	<u>Teslar</u>
Bag No.	<u>3</u>	Leak Checks	<u>OK</u>
Bag Vol.	<u>4</u> Liters	Posttest O ₂	<u>Reading</u>
		320 P No.	<u>NA</u>

Moisture Recovery Data:

Impinger No.	1	2	3	4	Desiccant	Total
Final Volume	206	68	4		1418	
Initial Volume	52	52	2		1410	
Difference	154	18	4		8	186

Field Computer Summary

Project Name: LP HAYWARD
Sampling Location: Line 2 core dryer out
Date of Test: 6-16-94
Test Number: 1

Operator M. Lofthus

Initialization Parameters	Run Specific Input Parameters <i>3 SURFACE DRY</i>			
	Run 1	Run 2	Run 3	Run 4
Meter Coef. - α = <u>1.0044</u>	VIO <u>343.43</u>	<u>387.00</u>		
Orif. Coef. - $\Delta H @$ = <u>1.689</u>	No. Of Points <u>12</u>	<u>220</u>	<u>12</u>	
Pitot Coef. - C_p = <u>835</u>	MC <u>24</u>	<u>22</u>		
Nozzle Dia. - D_n = <u>.200</u>	V/F <u>386.58</u>	<u>415.89</u>		
Bar. Pres. - P_b = <u>28.63</u>	Grams H_2O <u>185</u>	<u>161</u>		
Time/Point - ΔT = <u>5</u>	Run Time <u>60</u>	<u>60.36</u>	<u>60</u>	
Moisture Content = <u>24</u>	1-Rnd/2-Rect <u>1</u>	<u>1</u>	<u>1</u>	
% Oxygen = <u>17</u>	Diameter(Ins.) <u>41.75</u>	<u>41.75</u>	<u>41.75</u>	
Meter Temp. - t_m = <u>90</u>	Length(Ins.) <u>∞</u>	<u>∞</u>	<u>∞</u>	
Static Pres. - P_g = <u>-16.0</u>	Width(Ins.) <u>∞</u>	<u>∞</u>	<u>∞</u>	

End Of Run Summary

	Run 1	Run 2	Run 3	Run 4
Avg. $\sqrt{\Delta P}$ <u>1.301</u>	<u>1.433</u>			
Avg. ΔH <u>1.358</u>	<u>1.763</u>			
Avg. t_s <u>219.58</u>	<u>217.07</u>			
Avg. t_m <u>94.08</u>	<u>104.42</u>			
Standard Vol. <u>39.66</u>	<u>26.09</u>			
Moist. Content <u>18.00</u>	<u>22.51</u>			
Avg. Gas Vel. <u>89.60</u>	<u>97.67</u>			
% Isokinetic <u>96.47</u>	<u>101.90</u>			
ACFM <u>57106</u>	<u>55713</u>			
DSCFM <u>29873</u>	<u>31014</u>			

$T_m = 100$
 $P_g = -14.2$

EPA Method 5 Field Data Sheet

Project HP Hayward Train No. C71B4P3 Pitot Tube No. 2 Cp 835 Sampling Train Leak Checks:
 Sample Location Line 2 condenser out Meter Coef. @ 10044 Bar. Pres. 28.63 Ins. Hg Pretest 0.00 @ 15 Ins. Hg
 Date 6-16-94 Test 1 Run 1 Office Coef. ΔH@1659 Static Pres. -16 Ins. H₂O Posttest 0.01 @ 13.3 Ins. Hg
 Operators msl KJC Nozzle No. 3-L D_n 200 Estimated MC 24 % Pitot - Positive 0.0 Negative 0.0

Point No.	Time ΔT	Meter Vol. V _m Cubic Feet	Velocity Head - ΔP Inches WC	Orifice Meter - ΔH Inches WC	Desired ΔV _m	Desired V _m	Vacuum Inches Hg	Stack Temp. ° F	Sampling Train Temperatures - ° F					320 P Oxygen Percent
									Filter	Probe	Impinger Outlet	Meter Inlet	Meter Outlet	
A 6	5	347.65	2.45	1.91	424	767	7.2	216	250	245	66	95	99	
5	10	351.58	2.10	1.65	397	164	6.5	220	250	252	65	96	102	
4	15	355.40	1.90	1.50	378	542	6.5	221	249	249	63	96	105	
3	20	358.80	1.30	1.03	314	856	6.2	221	249	251	60	97	107	18.0
2	25	361.66	1.20	.95	303	158	5.1	220	249	251	60	98	107	17.8
1	30	364.57	1.20	.95	303	461	5.1	220	250	250	61	99	107	17.4
B 6	35	368.27	1.90	1.50	382	844	8.5	216	237	248	64	100	107	17.4
5	40	372.09	1.80	1.43	371	215	9.1	222	248	249	62	100	109	17.5
4	45	375.63	1.45	1.15	334	548	8.5	221	258	251	63	101	110	17.6
3	50	378.97	1.65	1.32	357	905	8.3	221	250	251	64	101	110	17.5
2	55	382.70	2.00	1.59	393	298	10.5	221	250	251	64	101	111	17.4
1	60	386.58	1.60	1.29	353	651	10.5	216	249	250	64	102	111	17.4
(1638)														

Samples Recovered: Filter No. 3109 ; ☒ Probe Wash; ☒ Wet Catch; ☐ Other

Integrated Gas Sampling Data:

Box No. 4 Bag Material Tedlar
 Bag No. 1 Leak Checks 0.00 cc/min. @ 25" Hg
 Bag Vol. 40 Liters Posttest O₂ Reading _____
 320 P No. _____

Moisture Recovery Data:

Impinger No.	1	2	3	4	Desiccant	Total
Final Volume	320	146	0	0	1489	
Initial Volume	100	100	0	0	1470	
Difference	126	46	0	0	13	185

EPA Method 5 Field Data Sheet

Project LP Hayward Train No. 67344P3 Pitot Tube No. 2 Cp 835 Sampling Train Leak Checks:
 Sample Location Stack Surface Inlet Meter Coef. 0.9944 Bar. Pres. 28.63 Ins. Hg Pretest 0.00 @ 15 Ins. Hg
 Date 6/10/94 Test 2 Run 1 Office Coef. ΔH@ 1.682 Static Pres. -14.2 Ins. H₂O Posttest 0.00 @ 17.1 Ins. Hg
 Operators MSL, KJR Nozzle No. 37 D_n 200 Estimated MC 22 % Pitot - Positive 2 Negative 0

Point No.	Time ΔT	Meter Vol. V _m Cubic Feet	Velocity Head - ΔP Inches WC	Orifice Meter - ΔH Inches WC	Desired ΔV _m	Desired V _m	Vacuum Inches Hg	Stack Temp. °F	Sampling Train Temperatures - °F					320 P Oxygen Percent
									Filter	Probe	Impinger Outlet	Meter Inlet	Meter Outlet	
A 10	3	389.58	2.40	2.00	262	962	6.5	216	246	246	64	99	102	18.0
9	6	392.00	2.05	1.71	242	204	5.9	217	248	244	63	99	103	18.2
8	9	394.77	2.50	2.14	231	476	7.2	218	251	248	62	99	106	18.0
7	12	397.17	2.20	1.87	254	730	6.8	220	252	252	62	99	108	17.3
6	15	399.75	2.25	1.92	258	988	7.6	219	250	252	63	100	108	18.2
5	18	402.20	1.80	1.54	231	218	7.4	218	249	250	64	100	109	18.0
4	21	404.55	1.85	1.59	235	453	7.4	215	248	250	64	100	110	18.4
3	24	406.74	1.70	1.46	225	678	7.1	217	249	250	64	101	110	18.2
2	27	408.92	1.70	1.47	226	803	7.1	214	250	250	64	101	110	18.3
1	30	411.06	1.50	1.29	211	115	7.1	217	250	250	64	101	111	18.1
B 18	33	413.49	2.30	1.97	261	376	11.5	220	249	247	63	102	111	17.9
9	36	416.89	2.55	2.18	275	651	16.0	221	250	248	63	102	111	17.7
8	39							2	2	2				
7	42								2	2				
6	45								2	2				
5	48								2	2				
4	51								2	2				
3	54								2	2				
2	57								2	2				
1	60								2	2				
(1814)														
36														
0=60		V _m = 29.89		ΔH = 1.763				T _s = 272.67					T _m = 60.42	

Samples Recovered: Filter No. 3084 ; ☒ Probe Wash; ☒ Wet Catch; ☐ Other

Integrated Gas Sampling Data:

Box No. 4 Bag Material Redlar
 Bag No. 2 Leak Checks 0.00 cc/min. @ 25" Hg
 Bag Vol. 40 Liters Posttest O₂ Reading _____
 320 P No. _____

Moisture Recovery Data:

1	2	3	4	Desiccant	Total
214	132	0	-	1320	
100	100	0	-	1361	
114	32	0	-	15	261

APPENDIX B
Laboratory Data and Reports

ORSAT ANALYTICAL DATA

EPA Method 3 Laboratory Summary Sheet

Project L.P. Hayward Analyst K. Lattery
 Sampling Location Line 1 Analysis Date 6-17-94
 Sampling Date 6-16-94 Apparatus Leak Check - Pos. 0.00 Neg. 0.00
 Project Number 940614.401 Apparatus Identification 03-01
 Sample Type ☒ Integrated ☐ Grab

Test No.	Run No.	Orsat Analyzer Results			F _o	O ₂ Analyzer Results		Sample Container
		% CO ₂	% O ₂	% CO		Field	Lab	
1	0	0.00	20.90		—			☐ Tedlar™ Bag ☐ Glass Bulb
1	2	4.00	17.00		0.975			☒ Tedlar™ Bag ☐ Glass Bulb
2	2	3.80	17.20		0.974			☒ Tedlar™ Bag ☐ Glass Bulb
1	2	3.80	17.00		1.026			☒ Tedlar™ Bag ☐ Glass Bulb
2	2	4.00	16.90		1.000			☒ Tedlar™ Bag ☐ Glass Bulb
								☐ Tedlar™ Bag ☐ Glass Bulb
								☐ Tedlar™ Bag ☐ Glass Bulb
								☐ Tedlar™ Bag ☐ Glass Bulb
								☐ Tedlar™ Bag ☐ Glass Bulb
								☐ Tedlar™ Bag ☐ Glass Bulb

Calculate F_o before evacuating any samples. Compare F_o to expected fuel values. If discrepancies exist, reanalyze samples. Calculate F_o as follows:

$$F_o = \frac{20.9 - \% O_2}{\% CO_2}$$

Comments Field + Lab O₂
Analyzer Results Not
Recorded Due To Inoperable
Analyzer Pump.

F _o Ranges For Common Fuels	
Anthracite Coal & Lignite	1.016 - 1.130
Bituminous Coal	1.083 - 1.230
Distillate Oil	1.260 - 1.413
Residual Oil	1.210 - 1.370
Wood	1.000 - 1.120
Wood Bark	1.003 - 1.130
Natural Gas	1.600 - 1.836
Propane	1.434 - 1.586
Butane	1.405 - 1.553

EPA Method 3 Laboratory Summary Sheet

Project L.P. Hayward Analyst K. Lattery
 Sampling Location Line 2 Analysis Date 6-17-94
 Sampling Date 6-16-94 Apparatus Leak Check - Pos. 0.00 Neg. 0.00
 Project Number 940614.401 Apparatus Identification 03-01
 Sample Type ☒ Integrated ☐ Grab

Test No.	Run No.	Orsat Analyzer Results			F ₀	O ₂ Analyzer Results		Sample Container
		% CO ₂	% O ₂	% CO		Field	Lab	
1	0	0.00	20.90		—			☐ Tedlar™ Bag ☐ Glass Bulb
1	1	2.20	18.80		0.955			☒ Tedlar™ Bag ☐ Glass Bulb
2	1	2.80	18.20		0.964			☒ Tedlar™ Bag ☐ Glass Bulb
3	1	2.80	18.40		0.893			☒ Tedlar™ Bag ☐ Glass Bulb
1	1	3.60	17.60		0.917			☒ Tedlar™ Bag ☐ Glass Bulb
2	1	3.00	18.00		0.967			☒ Tedlar™ Bag ☐ Glass Bulb
								☐ Tedlar™ Bag ☐ Glass Bulb
								☐ Tedlar™ Bag ☐ Glass Bulb
								☐ Tedlar™ Bag ☐ Glass Bulb
								☐ Tedlar™ Bag ☐ Glass Bulb

Calculate F₀ before evacuating any samples. Compare F₀ to expected fuel values. If discrepancies exist, reanalyze samples. Calculate F₀ as follows:

$$F_0 = \frac{20.9 - \% O_2}{\% CO_2}$$

Comments Field + Lab O₂
Analyzer Results Not
Recorded Due To Inoperable
Analyzer Pump.

F ₀ Ranges For Common Fuels	
Anthracite Coal & Lignite	1.016 - 1.130
Bituminous Coal	1.083 - 1.230
Distillate Oil	1.260 - 1.413
Residual Oil	1.210 - 1.370
Wood	1.000 - 1.120
Wood Bark	1.003 - 1.130
Natural Gas	1.600 - 1.836
Propane	1.434 - 1.586
Butane	1.405 - 1.553

EPA Method 3 Laboratory Data Sheet

Project L.P. Hayward Analyst K. Lattery
 Sampling Location Line 1 Analysis Date 6-17-94
 Sampling Date 6-16-94 Apparatus Leak Check - Pos. 0.00 Neg. 0.00
 Project Number 940614.401 Apparatus Identification 08-01

Test <u>1</u> Run <u>0</u>	Aliquot Volume Zero Point <u>0.00</u> ml Sample Volume <u>100.00</u> ml	CO₂ Initial Reading <u>0.00</u> ml Final Reading <u>0.00</u> ml Volume CO ₂ <u>0.00</u> ml % CO ₂ <u>0.00</u> %	O₂ Initial Reading <u>0.00</u> ml Final Reading <u>20.90</u> ml Volume O ₂ <u>20.90</u> ml % O ₂ <u>20.90</u> %
Duplicate	Aliquot Volume Zero Point _____ ml Sample Volume _____ ml	CO₂ Initial Reading _____ ml Final Reading _____ ml Volume CO ₂ _____ ml % CO ₂ _____ %	O₂ Initial Reading _____ ml Final Reading _____ ml Volume O ₂ _____ ml % O ₂ _____ %
Average		% CO ₂ <u>0.00</u> %	% O ₂ <u>20.90</u> %
Test <u>1</u> Run <u>2</u> <u>EFB OUTLET</u>	Aliquot Volume Zero Point <u>0.00</u> ml Sample Volume <u>100.00</u> ml	CO₂ Initial Reading <u>0.00</u> ml Final Reading <u>4.00</u> ml Volume CO ₂ <u>4.00</u> ml % CO ₂ <u>4.00</u> %	O₂ Initial Reading <u>4.00</u> ml Final Reading <u>21.00</u> ml Volume O ₂ <u>17.00</u> ml % O ₂ <u>17.00</u> %
Duplicate	Aliquot Volume Zero Point <u>0.00</u> ml Sample Volume <u>100.00</u> ml	CO₂ Initial Reading <u>0.00</u> ml Final Reading <u>4.00</u> ml Volume CO ₂ <u>4.00</u> ml % CO ₂ <u>4.00</u> %	O₂ Initial Reading <u>4.00</u> ml Final Reading <u>21.00</u> ml Volume O ₂ <u>17.00</u> ml % O ₂ <u>17.00</u> %
Average		% CO ₂ <u>4.00</u> %	% O ₂ <u>17.00</u> %

Comments: _____

EPA Method 3 Laboratory Data Sheet

Project L.P. Hayward Analyst K. Lattery
 Sampling Location Line 1 Analysis Date 6-17-94
 Sampling Date 6-16-94 Apparatus Leak Check - Pos. 0.00 Neg. 0.00
 Project Number 940614.401 Apparatus Identification 08-01

Test <u>2</u> Run <u>2</u> EFB OUTLET	Aliquot Volume Zero Point <u>0.00</u> ml Sample Volume <u>100.00</u> ml	CO ₂ Initial Reading <u>0.00</u> ml Final Reading <u>3.80</u> ml Volume CO ₂ <u>3.80</u> ml % CO ₂ <u>3.80</u> %	O ₂ Initial Reading <u>3.80</u> ml Final Reading <u>21.00</u> ml Volume O ₂ <u>17.20</u> ml % O ₂ <u>17.20</u> %
Duplicate	Aliquot Volume Zero Point <u>0.00</u> ml Sample Volume <u>100.00</u> ml	CO ₂ Initial Reading <u>0.00</u> ml Final Reading <u>3.80</u> ml Volume CO ₂ <u>3.80</u> ml % CO ₂ <u>3.80</u> %	O ₂ Initial Reading <u>3.80</u> ml Final Reading <u>21.00</u> ml Volume O ₂ <u>17.20</u> ml % O ₂ <u>17.20</u> %
Average		% CO ₂ <u>3.80</u> %	% O ₂ <u>17.20</u> %
Test <u>1</u> Run <u>2</u> CORE DRYER OUTLET	Aliquot Volume Zero Point <u>0.00</u> ml Sample Volume <u>100.00</u> ml	CO ₂ Initial Reading <u>0.00</u> ml Final Reading <u>3.80</u> ml Volume CO ₂ <u>3.80</u> ml % CO ₂ <u>3.80</u> %	O ₂ Initial Reading <u>3.80</u> ml Final Reading <u>20.80</u> ml Volume O ₂ <u>17.00</u> ml % O ₂ <u>17.00</u> %
Duplicate	Aliquot Volume Zero Point <u>0.00</u> ml Sample Volume <u>100.00</u> ml	CO ₂ Initial Reading <u>0.00</u> ml Final Reading <u>3.80</u> ml Volume CO ₂ <u>3.80</u> ml % CO ₂ <u>3.80</u> %	O ₂ Initial Reading <u>3.80</u> ml Final Reading <u>20.80</u> ml Volume O ₂ <u>17.00</u> ml % O ₂ <u>17.00</u> %
Average		% CO ₂ <u>3.80</u> %	% O ₂ <u>17.00</u> %

Comments: _____

EPA Method 3 Laboratory Data Sheet

Project L.P. Hayward Analyst K. Lattery
 Sampling Location Line 1 Analysis Date 6-17-94
 Sampling Date 6-16-94 Apparatus Leak Check - Pos. 0.00 Neg. 0.00
 Project Number 940614.401 Apparatus Identification 08-01

Test <u>2</u> Run <u>2</u> SURFACE DRYER OUTLET	Aliquot Volume Zero Point <u>0.00</u> ml Sample Volume <u>100.00</u> ml	CO ₂ Initial Reading <u>2.00</u> ml Final Reading <u>4.00</u> ml Volume CO ₂ <u>4.00</u> ml % CO ₂ <u>4.00</u> %	O ₂ Initial Reading <u>4.00</u> ml Final Reading <u>20.90</u> ml Volume O ₂ <u>16.90</u> ml % O ₂ <u>16.90</u> %
Duplicate	Aliquot Volume Zero Point <u>0.00</u> ml Sample Volume <u>100.00</u> ml	CO ₂ Initial Reading <u>0.00</u> ml Final Reading <u>4.00</u> ml Volume CO ₂ <u>4.00</u> ml % CO ₂ <u>4.00</u> %	O ₂ Initial Reading <u>4.00</u> ml Final Reading <u>20.90</u> ml Volume O ₂ <u>16.90</u> ml % O ₂ <u>16.90</u> %
Average		% CO ₂ <u>4.00</u> %	% O ₂ <u>16.90</u> %
Test ____ Run ____	Aliquot Volume Zero Point _____ ml Sample Volume _____ ml	CO ₂ Initial Reading _____ ml Final Reading _____ ml Volume CO ₂ _____ ml % CO ₂ _____ %	O ₂ Initial Reading _____ ml Final Reading _____ ml Volume O ₂ _____ ml % O ₂ _____ %
Duplicate	Aliquot Volume Zero Point _____ ml Sample Volume _____ ml	CO ₂ Initial Reading _____ ml Final Reading _____ ml Volume CO ₂ _____ ml % CO ₂ _____ %	O ₂ Initial Reading _____ ml Final Reading _____ ml Volume O ₂ _____ ml % O ₂ _____ %
Average		% CO ₂ _____ %	% O ₂ _____ %

Comments: _____

EPA Method 3 Laboratory Data Sheet

Project L.P. Hayward Analyst K. Lat tery
 Sampling Location Line 2 Analysis Date 6-17-94
 Sampling Date 6-16-94 Apparatus Leak Check - Pos. 0.00 Neg. 0.00
 Project Number 940614.401 Apparatus Identification 06-01

Test <u>1</u> Run <u>0</u> <i>EL</i>	Aliquot Volume Zero Point <u>0.00</u> ml Sample Volume <u>100.00</u> ml	CO ₂ Initial Reading <u>0.00</u> ml Final Reading <u>0.00</u> ml Volume CO ₂ <u>0.00</u> ml % CO ₂ <u>0.00</u> %	O ₂ Initial Reading <u>0.00</u> ml Final Reading <u>20.90</u> ml Volume O ₂ <u>20.90</u> ml % O ₂ <u>20.90</u> %
Duplicate	Aliquot Volume Zero Point _____ ml Sample Volume _____ ml	CO ₂ Initial Reading _____ ml Final Reading _____ ml Volume CO ₂ _____ ml % CO ₂ _____ %	O ₂ Initial Reading _____ ml Final Reading _____ ml Volume O ₂ _____ ml % O ₂ _____ %
Average		% CO ₂ <u>0.00</u> %	% O ₂ <u>20.90</u> %
Test <u>1</u> Run <u>1</u> <i>EPB OUTLET</i>	Aliquot Volume Zero Point <u>0.00</u> ml Sample Volume <u>100.00</u> ml	CO ₂ Initial Reading <u>0.00</u> ml Final Reading <u>2.20</u> ml Volume CO ₂ <u>2.20</u> ml % CO ₂ <u>2.20</u> %	O ₂ Initial Reading <u>2.20</u> ml Final Reading <u>21.00</u> ml Volume O ₂ <u>18.80</u> ml % O ₂ <u>18.80</u> %
Duplicate	Aliquot Volume Zero Point <u>0.00</u> ml Sample Volume <u>100.00</u> ml	CO ₂ Initial Reading <u>0.00</u> ml Final Reading <u>2.20</u> ml Volume CO ₂ <u>2.20</u> ml % CO ₂ <u>2.20</u> %	O ₂ Initial Reading <u>2.20</u> ml Final Reading <u>21.00</u> ml Volume O ₂ <u>18.80</u> ml % O ₂ <u>18.80</u> %
Average		% CO ₂ <u>2.20</u> %	% O ₂ <u>18.80</u> %

Comments: _____

EPA Method 3 Laboratory Data Sheet

Project L.P. Hayward Analyst K. Lattery
 Sampling Location Line 2 Analysis Date 6-17-94
 Sampling Date 6-16-94 Apparatus Leak Check - Pos. 0.00 Neg. 0.00
 Project Number 940614.401 Apparatus Identification 0B-01

Test <u>2</u> Run <u>1</u> EFB OUTLET	Aliquot Volume Zero Point <u>0.00</u> ml	CO ₂ Initial Reading <u>0.00</u> ml Final Reading <u>2.80</u> ml Volume CO ₂ <u>2.80</u> ml % CO ₂ <u>2.80</u> %	O ₂ Initial Reading <u>2.80</u> ml Final Reading <u>21.00</u> ml Volume O ₂ <u>18.20</u> ml % O ₂ <u>18.20</u> %
	Sample Volume <u>100.00</u> ml		
Duplicate	Aliquot Volume Zero Point <u>0.00</u> ml	CO ₂ Initial Reading <u>0.00</u> ml Final Reading <u>2.80</u> ml Volume CO ₂ <u>2.80</u> ml % CO ₂ <u>2.80</u> %	O ₂ Initial Reading <u>2.80</u> ml Final Reading <u>21.00</u> ml Volume O ₂ <u>18.20</u> ml % O ₂ <u>18.20</u> %
	Sample Volume <u>100.00</u> ml		
Average		% CO ₂ <u>2.80</u> %	% O ₂ <u>18.20</u> %
Test <u>3</u> Run <u>1</u> EFB OUTLET	Aliquot Volume Zero Point <u>0.00</u> ml	CO ₂ Initial Reading <u>0.00</u> ml Final Reading <u>2.80</u> ml Volume CO ₂ <u>2.80</u> ml % CO ₂ <u>2.80</u> %	O ₂ Initial Reading <u>2.80</u> ml Final Reading <u>21.20</u> ml Volume O ₂ <u>18.40</u> ml % O ₂ <u>18.40</u> %
	Sample Volume <u>100.00</u> ml		
Duplicate	Aliquot Volume Zero Point <u>0.00</u> ml	CO ₂ Initial Reading <u>0.00</u> ml Final Reading <u>2.80</u> ml Volume CO ₂ <u>2.80</u> ml % CO ₂ <u>2.80</u> %	O ₂ Initial Reading <u>2.80</u> ml Final Reading <u>21.20</u> ml Volume O ₂ <u>18.40</u> ml % O ₂ <u>18.40</u> %
	Sample Volume <u>100.00</u> ml		
Average		% CO ₂ <u>2.80</u> %	% O ₂ <u>18.40</u> %

Comments: _____

EPA Method 3 Laboratory Data Sheet

Project L.R. Hayward Analyst K. Lattery
 Sampling Location Line 2 Analysis Date 6-17-94
 Sampling Date 6-16-94 Apparatus Leak Check - Pos. 0.00 Neg. 0.00
 Project Number 940614.401 Apparatus Identification 08-01

Test <u>1</u> Run <u>1</u> CORE DRYER OUTLET	Aliquot Volume Zero Point <u>0.00</u> ml Sample Volume <u>100.00</u> ml	CO ₂ Initial Reading <u>0.00</u> ml Final Reading <u>3.60</u> ml Volume CO ₂ <u>3.60</u> ml % CO ₂ <u>3.60</u> %	O ₂ Initial Reading <u>3.60</u> ml Final Reading <u>21.20</u> ml Volume O ₂ <u>17.60</u> ml % O ₂ <u>17.60</u> %
Duplicate	Aliquot Volume Zero Point <u>0.00</u> ml Sample Volume <u>100.00</u> ml	CO ₂ Initial Reading <u>0.00</u> ml Final Reading <u>3.60</u> ml Volume CO ₂ <u>3.60</u> ml % CO ₂ <u>3.60</u> %	O ₂ Initial Reading <u>3.60</u> ml Final Reading <u>21.20</u> ml Volume O ₂ <u>17.60</u> ml % O ₂ <u>17.60</u> %
Average		% CO ₂ <u>3.60</u> %	% O ₂ <u>17.60</u> %
Test <u>2</u> Run <u>1</u> SURFACE DRYER OUTLET	Aliquot Volume Zero Point <u>0.00</u> ml Sample Volume <u>100.00</u> ml	CO ₂ Initial Reading <u>0.00</u> ml Final Reading <u>3.00</u> ml Volume CO ₂ <u>3.00</u> ml % CO ₂ <u>3.00</u> %	O ₂ Initial Reading <u>3.00</u> ml Final Reading <u>21.00</u> ml Volume O ₂ <u>18.00</u> ml % O ₂ <u>18.00</u> %
Duplicate	Aliquot Volume Zero Point <u>0.00</u> ml Sample Volume <u>100.00</u> ml	CO ₂ Initial Reading <u>0.00</u> ml Final Reading <u>3.00</u> ml Volume CO ₂ <u>3.00</u> ml % CO ₂ <u>3.00</u> %	O ₂ Initial Reading <u>3.00</u> ml Final Reading <u>21.00</u> ml Volume O ₂ <u>18.00</u> ml % O ₂ <u>18.00</u> %
Average		% CO ₂ <u>3.00</u> %	% O ₂ <u>18.00</u> %

Comments: _____

PARTICULATE ANALYTICAL DATA

EPA Method 5 Particulate Gravimetric Sheet

Inorganic Residuals

Project LOUISIANA PACIFIC Analyst KAB
 Sampling Location DRYERS OUT Analysis Date(s) 6/17, 6/18, 6/20, 6/21/94
 Sampling Date 6/15/94 Sampling Reagent _____
 Test Number T1, T2 LDMS Entry _____ Initials _____
 Project Number 940617.500 LDMS Validation 6.22.94 Initials me

Sample No. 13077.0
 Run Number TIR1
 Dish Number 50

Date/Time 6/21/94 0830
 Gross Weight 115.3897 g

Date/Time 6/21/94 1445
 Gross Weight 115.3892 g

Avg. Gross Wt. 115.3894 g
 Dish Tare Wt. 115.2820 g
 Difference 0.1074 g

Blank Weight 0.0007 g

Inorganic Residuals Wt. 0.1067 g

Transfer "Inorganic Residuals Wt." to Box Number 1.

WC 1 0.1067 g

Sample No. 13078.8
 Run Number TIR2
 Dish Number B4

Date/Time 6/21/94 0830
 Gross Weight 103.7664 g

Date/Time 6/21/94 1445
 Gross Weight 103.2666 g

Avg. Gross Wt. 103.2665 g
 Dish Tare Wt. 103.2058 g
 Difference 0.0607 g

Blank Weight 0.0007 g

Inorganic Residuals Wt. 0.0600 g

Transfer "Inorganic Residuals Wt." to Box Number 2.

WC 2 0.0600 g

Sample No. 13079.6
 Run Number TIR1
 Dish Number MOJER

Date/Time 6/21/94 0830
 Gross Weight 104.5774 g

Date/Time 6/21/94 1445
 Gross Weight 104.5769 g

Avg. Gross Wt. 104.5772 g
 Dish Tare Wt. 104.5198 g
 Difference 0.0574 g

Blank Weight 0.0007 g
0.0567 g ^{KAB}

Inorganic Residuals Wt. 0.0567 g

Transfer "Inorganic Residuals Wt." to Box Number 3.

WC 3 0.0567 g

EPA Method 5 Particulate Gravimetric Sheet
Organic Condensibles

Project LOUISIANA PACIFIC Analyst KAB
Sampling Location DRYERS OUT Analysis Date(s) 6/17, 6/18, 6/20, 6/21/94
Sampling Date 6/15/94 Sampling Reagent _____
Test Number T1, T2 LDMS Entry _____ Initials _____
Project Number 940617.500 LDMS Validation 10-22 94 Initials Jme

Sample No. <u>13077.0</u>	Sample No. <u>13078.8</u>	Sample No. <u>13079.6</u>
Run Number <u>TIR1</u>	Run Number <u>TIR2</u>	Run Number <u>TIR1</u>
Dish Number <u>SLP</u>	Dish Number <u>FE</u>	Dish Number <u>PO</u>
Date/Time <u>6/21/94 0830</u>	Date/Time <u>6/21/94 0830</u>	Date/Time <u>6/21/94 0830</u>
Gross Weight <u>105.0826</u> g	Gross Weight <u>115.9293</u> g	Gross Weight <u>116.8586</u> g ^{KAB 6/21/94} <u>116.8846</u>
Date/Time <u>6/21/94 1445</u>	Date/Time <u>6/21/94 1445</u>	Date/Time <u>6/21/94 1445</u>
Gross Weight <u>105.0823</u> g	Gross Weight <u>115.9289</u> g	Gross Weight <u>116.8842</u> g
Avg. Gross Wt. <u>105.0824</u> g	Avg. Gross Wt. <u>115.9291</u> g	Avg. Gross Wt. <u>116.8844</u> g
Dish Tare Wt. <u>105.0343</u> g	Dish Tare Wt. <u>115.9018</u> g	Dish Tare Wt. <u>116.8586</u> g
Difference <u>0.0481</u> g	Difference <u>0.0273</u> g	Difference <u>0.0258</u> g
Blank Weight <u>0.0002</u> g	Blank Weight <u>0.0002</u> g	Blank Weight <u>0.0002</u> g ^{KAB 6/21/94} <u>0.0256</u>
Condensible Organic Wt. <u>0.0479</u> g	Condensible Organic Wt. <u>0.0271</u> g	Condensible Organic Wt. <u>0.0256</u> g
Transfer "Condensible Organic Wt." to Box Number 1.	Transfer "Condensible Organic Wt." to Box Number 2.	Transfer "Condensible Organic Wt." to Box Number 3.
WC 1 <u>0.0479</u> g	WC 2 <u>0.0271</u> g	WC 3 <u>0.0256</u> g

EPA Method 5 Particulate Gravimetric Sheet

Particulate In Probe Wash

Project LOUISIANA PACIFIC Analyst KAB
 Sampling Location DEYER'S OLT Analysis Date(s) 6/17/94, 6/18/94, 6/20/94
 Sampling Date 6/15/94 Cleanup Reagent(s) _____
 Test Number T1.72 LDMS Entry _____ Initials _____
 Project Number 940617.500 LDMS Validation 6.22.94 Initials me

Sample No. <u>13077.0</u>	Sample No. <u>13778.8</u>	Sample No. <u>13079.6</u>
Run Number <u>TIR1</u>	Run Number <u>TIR2</u>	Run Number <u>TIR31</u>
Dish Number <u>B10</u>	Dish Number <u>8</u>	Dish Number <u>B2</u>
Reagent Vol. <u>175</u> ml	Reagent Vol. <u>175</u> ml	Reagent Vol. <u>10</u> ml
Date/Time <u>6/18/94 1600</u>	Date/Time <u>6/18/94 1600</u>	Date/Time <u>6/18/94 1600</u>
Gross Weight <u>103.2642</u> g	Gross Weight <u>103.0805</u> g	Gross Weight <u>103.9253</u> g
Date/Time <u>6/20/94 0830</u>	Date/Time <u>6/20/94 0830</u>	Date/Time <u>6/18/94 0830</u>
Gross Weight <u>103.2647</u> g	Gross Weight <u>103.0806</u> g	Gross Weight <u>103.9258</u> g
Avg. Gross Wt. <u>103.2644</u> g	Avg. Gross Wt. <u>103.0806</u> g	Avg. Gross Wt. <u>103.9256</u> g
Dish Tare Wt. <u>103.18285</u> g	Dish Tare Wt. <u>103.0201</u> g	Dish Tare Wt. <u>103.9185</u> g
Difference <u>0.0819</u> g	Difference <u>0.0605</u> g	Difference <u>0.0071</u> g
Blank Weight <u>0.001</u> g	Blank Weight <u>0.001</u> g	Blank Weight <u>0.001</u> g
Particulate In Rinse Weight <u>0.0809</u> g	Particulate In Rinse Weight <u>0.0595</u> g	Particulate In Rinse Weight <u>0.0061</u> g
Transfer "Particulate In Rinse Weight" to Box Number 1.	Transfer "Particulate In Rinse Weight" to Box Number 2.	Transfer "Particulate In Rinse Weight" to Box Number 3.
PW 1 <u>0.0809</u> g	PW 2 <u>0.0595</u> g	PW 3 <u>0.0061</u> g

EPA Method 5 Particulate Gravimetric Sheet

Particulate On Filter

Project LOUISIANA PACIFIC Analyst KAB
Sampling Location DRYERS COT Analysis Date(s) 6/17/94
Sampling Date 6/15/94 Filter Type FIBERGLASS & METAL TUBE
Test Number T1, T2 LDMS Entry _____ Initials _____
Project Number 940617.500 LDMS Validation 6.22-94 Initials me

Sample No. <u>13077.0</u>	Sample No. <u>13078.8</u>	Sample No. <u>13079.6</u>
Run Number <u>TIR1</u>	Run Number <u>TIR2</u>	Run Number <u>TIR1</u>
Filter Number <u>3109</u>	Filter Number <u>3216</u>	Filter Number <u>P11</u>
Date/Time <u>6/17/94 1630</u>	Date/Time <u>6/17/94 1630</u>	Date/Time <u>6/17/94 1630</u>
Gross Weight <u>1.0600</u> g	Gross Weight <u>0.8698</u> g	Gross Weight <u>42.7528</u> g
Date/Time _____	Date/Time _____	Date/Time _____
Gross Weight _____ g	Gross Weight _____ g	Gross Weight _____ g
Avg. Gross Wt. <u>1.0600</u> g	Avg. Gross Wt. <u>0.8698</u> g	Avg. Gross Wt. <u>42.7528</u> g
Filter Tare Wt. <u>0.66760</u> g	Filter Tare Wt. <u>0.66326</u> g	Filter Tare Wt. <u>42.6193</u> g
Difference <u>0.3924</u> g	Difference <u>0.2065</u> g	Difference <u>0.1335</u> g
Particulate On Filter Weight <u>0.3924</u> g	Particulate On Filter Weight <u>0.2065</u> g	Particulate On Filter Weight <u>0.1335</u> g
Transfer "Particulate On Filter Weight" to Box Number 1.	Transfer "Particulate On Filter Weight" to Box Number 2.	Particulate On Filter Weight" to Box Number 3.
Sum particulate weights from each box labeled "1" and record in box labeled "T1."	Sum particulate weights from each box labeled "2" and record in box labeled "T2."	Sum particulate weights from each box labeled "3" and record in box labeled "T3."
AF 1 <u>0.3924</u> g	AF 2 <u>0.2065</u> g	AF 3 <u>0.1335</u> g
Total T1 <u>0.6279</u> g	Total T2 <u>0.3531</u> g	Total T3 <u>0.2219</u> g

EPA Method 5 Particulate Gravimetric Sheet

Reagent Blanks

Project LOUISIANA PACIFIC
Sampling Location DRYERS OUT
Sampling Date 6/15/94
Test Number T1, T2
Project Number 940617.500

Analyst KAB
Analysis Date(s) 6/17/94, 6/18, 6/20, 6/21

Wet Catch

Type: ☒ Organic Condensibles (Extract.)
☐ Inorganic (Residual)
☐ Other _____
☐ Retain For Further Analyses

Reagent 160
Volume 200 ml

Date/Time 6/21/94 0830
Gross Weight 105.114.3205 g

Date/Time 6/21/94 1445
Gross Weight 114.3206 g

Avg. Gross Wt. 114.3206 g

Dish Tare Wt. 114.3204 g

Difference 0.0002 g

Blank Weight 0.0002 g

Probe Wash

Type: ☒ Gravimetric
☐ Other _____
☐ Retain For Further Analyses

Reagent _____
Volume 200 ml

Date/Time 6/18/94 1600
Gross Weight 105.3115 g

Date/Time 6/20/94 0830
Gross Weight 105.3112 g

Avg. Gross Wt. 105.3114 g

Dish Tare Wt. 105.3104 g

Difference 0.0010 g

Blank Weight 0.0010 g

EPA Method 5 Particulate Gravimetric Sheet

Reagent Blanks

Project _____ Analyst _____
 Sampling Location _____ Analysis Date(s) _____
 Sampling Date _____
 Test Number _____
 Project Number _____

Wet Catch

Type: ☐ Organic Condensibles (Extract.)
☒ Inorganic (Residual)
☐ Other _____
☐ Retain For Further Analyses
 TOB

Reagent _____
 Volume _____ ml

Date/Time 6/21/94 0830
 Gross Weight 108.6231 g

Date/Time 6/21/94 1445
 Gross Weight 108.62248 g

Avg. Gross Wt. 108.6236 g

Dish Tare Wt. 108.6223 g

Difference +0.0007 g

Blank Weight .0007 g

Probe Wash

Type: ☒ Gravimetric
☐ Other _____
☐ Retain For Further Analyses

Reagent _____
 Volume _____ ml

Date/Time _____
 Gross Weight _____ g

Date/Time _____
 Gross Weight _____ g

Avg. Gross Wt. _____ g

Dish Tare Wt. _____ g

Difference _____ g

Blank Weight _____ g

EPA Method 5 Particulate Gravimetric Sheet
Reagent Blanks

Project _____ Analyst _____
Sampling Location _____ Analysis Date(s) _____
Sampling Date _____
Test Number _____
Project Number _____

Wet Catch

Type: ☐ Organic Condensibles (Extract.)
☒ Inorganic (Residual)
☐ Other _____
☐ Retain For Further Analyses

10B

Reagent _____
Volume _____ ml

Date/Time 6/21/94 0830
Gross Weight 108.6231 g

Date/Time 6/21/94 1445
Gross Weight 108.62248 g

Avg. Gross Wt. 108.6236 g
Dish Tare Wt. 108.6223 g
Difference +0.0007 g

Blank Weight .0007 g

Probe Wash

Type: ☒ Gravimetric
☐ Other _____
☐ Retain For Further Analyses

Reagent _____
Volume _____ ml

Date/Time _____
Gross Weight _____ g

Date/Time _____
Gross Weight _____ g

Avg. Gross Wt. _____ g
Dish Tare Wt. _____ g
Difference _____ g

Blank Weight _____ g

EPA Method 5 Particulate Gravimetric Sheet

Inorganic Residuals

Project LOUISIANA PACIFIC Analyst KAB
 Sampling Location DRYER OUT Analysis Date(s) 6/17, 6/18, 6/20, 6/21/94
 Sampling Date 6/15/94 Sampling Reagent _____
 Test Number T1, T2 LDMS Entry _____ Initials _____
 Project Number 940617.500 LDMS Validation 6-22-94 Initials gme

Sample No. 13085.0
 Run Number T2R1
 Dish Number Z4

Date/Time 6/21/94 0830
 Gross Weight 98.2750 g

Date/Time 6/21/94 1445
 Gross Weight 98.2745 g

Avg. Gross Wt. 98.2748 g
 Dish Tare Wt. 98.2284 g
 Difference 0.0464 g

Blank Weight 0.0007 g

Inorganic Residuals Wt. 0.0457 g

Transfer "Inorganic Residuals Wt." to Box Number 1.

WC 1 0.0457 g

Sample No. 13086.9
 Run Number T2R2
 Dish Number ATP

Date/Time 6/21/94 0830
 Gross Weight 100.7512 g
100.7715

Date/Time 6/21/94 1
 Gross Weight 100.7710 g

Avg. Gross Wt. 100.7712 g
 Dish Tare Wt. 100.6966 g
 Difference 0.0746 g

Blank Weight 0.0007 g

Inorganic Residuals Wt. 0.0739 g

Transfer "Inorganic Residuals Wt." to Box Number 2.

WC 2 0.0739 g

Sample No. _____
 Run Number _____
 Dish Number _____

Date/Time _____
 Gross Weight _____ g

Date/Time _____
 Gross Weight _____ g

Avg. Gross Wt. _____ g
 Dish Tare Wt. _____ g
 Difference _____ g

Blank Weight _____ g

Inorganic Residuals Wt. _____ g

Transfer "Inorganic Residuals Wt." to Box Number 3.

WC 3 _____ g

EPA Method 5 Particulate Gravimetric Sheet

Organic Condensibles

Project LOUISIANA PACIFIC Analyst KAB
 Sampling Location DRYER'S OUT Analysis Date(s) 6/17, 6/18, 6/20, 6/21/94
 Sampling Date 6/15/94 Sampling Reagent _____
 Test Number T1, T2 LDMS Entry _____ Initials _____
 Project Number 940617.500 LDMS Validation 6.22.94 Initials JK

Sample No. <u>13085.0</u>	Sample No. <u>13086.9</u>	Sample No. _____
Run Number <u>T2R1</u>	Run Number <u>T2R2</u>	Run Number _____
Dish Number <u>702</u>	Dish Number <u>JOSE</u>	Dish Number _____
Date/Time <u>6/21/94 0830</u>	Date/Time <u>6/21/94 0830</u>	Date/Time _____
Gross Weight <u>98.9646</u> g	Gross Weight <u>103.0697</u> g	Gross Weight _____ g
Date/Time <u>6/21/94 1445</u>	Date/Time <u>6/21/94 1445</u>	Date/Time _____
Gross Weight <u>98.9641</u> g	Gross Weight <u>103.0693</u> g	Gross Weight _____ g
Avg. Gross Wt. <u>98.9644</u> g	Avg. Gross Wt. <u>103.0695</u> g	Avg. Gross Wt. _____ g
Dish Tare Wt. <u>98.9497</u> g	Dish Tare Wt. <u>103.0413</u> g	Dish Tare Wt. _____ g
Difference <u>0.0147</u> g	Difference <u>0.0282</u> g	Difference _____ g
Blank Weight <u>0.0002</u> g	Blank Weight <u>0.0002</u> g	Blank Weight <u>0.0002</u> g
Condensible Organic Wt. <u>0.0145</u> g	Condensible Organic Wt. <u>0.0280</u> g	Condensible Organic Wt. _____ g
Transfer "Condensible Organic Wt." to Box Number 1.	Transfer "Condensible Organic Wt." to Box Number 2.	Transfer "Condensible Organic Wt." to Box Number 3.
WC 1 <u>0.0145</u> g	WC 2 <u>0.0280</u> g	WC 3 _____ g

EPA Method 5 Particulate Gravimetric Sheet

Particulate In Probe Wash

Project LOUISIANA PACIFIC Analyst KAS
Sampling Location DEYERS OUT Analysis Date(s) 6/17, 6/18, 6/20/94
Sampling Date 6/15/94 Cleanup Reagent(s) _____
Test Number T1, RT2 LDMS Entry _____ Initials _____
Project Number 940617.500 LDMS Validation 6.2294 Initials JMC

Sample No. 13085.0
Run Number T2R1
Dish Number 14
Reagent Vol. 10 ml

Date/Time 6/18/94 1600
Gross Weight 101.4620 g

Date/Time 6/20/94 0830
Gross Weight 101.4624 g

Avg. Gross Wt. 101.4622 g
Dish Tare Wt. 101.4555 g
Difference 0.0067 g

Blank Weight 0.001 g

Particulate In Rinse Weight 0.0057 g

Transfer "Particulate In Rinse Weight" to Box Number 1.

PW 1 0.0057 g

Sample No. 13086.9
Run Number T2R2
Dish Number REM
Reagent Vol. 10 ml

Date/Time 6/18/94 1600
Gross Weight 114.2088 g

Date/Time 6/20/94 0830
Gross Weight 114.2092 g

Avg. Gross Wt. 114.2090 g
Dish Tare Wt. 114.2011 g
Difference 0.0079 g

Blank Weight 0.001 g

Particulate In Rinse Weight 0.0069 g

Transfer "Particulate In Rinse Weight" to Box Number 2.

PW 2 0.0069 g

Sample No. _____
Run Number _____
Dish Number _____
Reagent Vol. _____ ml

Date/Time _____
Gross Weight _____ g

Date/Time _____
Gross Weight _____ g

Avg. Gross Wt. _____ g
Dish Tare Wt. _____ g
Difference _____ g

Blank Weight _____ g

Particulate In Rinse Weight _____ g

Transfer "Particulate In Rinse Weight" to Box Number 3.

PW 3 _____ g

EPA Method 5 Particulate Gravimetric Sheet

Particulate On Filter

Project LOUISIANA PACIFIC Analyst KAB
 Sampling Location DRYER OUT Analysis Date(s) 6/17/94
 Sampling Date 6/15/94 Filter Type FIBERGLASS, METAL THIMBEL
 Test Number T1, T2 LDMS Entry _____ Initials _____
 Project Number 940617.500 LDMS Validation 6-22-94 Initials [Signature]

Sample No. <u>13085.0</u>	Sample No. <u>13086.9</u>	Sample No. _____
Run Number <u>T2R1</u>	Run Number <u>T2R2</u>	Run Number _____
Filter Number <u>P14</u>	Filter Number <u>P10</u>	Filter Number _____
Date/Time <u>6/17/94 1630</u>	Date/Time <u>6/17/94 1630</u>	Date/Time _____
Gross Weight <u>40.8700</u> g	Gross Weight <u>43.3157</u> g	Gross Weight _____ g
Date/Time _____	Date/Time _____	Date/Time _____
Gross Weight _____ g	Gross Weight _____ g	Gross Weight _____ g
Avg. Gross Wt. <u>40.8700</u> g	Avg. Gross Wt. <u>43.3157</u> g	Avg. Gross Wt. _____ g
Filter Tare Wt. <u>40.8019</u> g	Filter Tare Wt. <u>43.1702</u> g	Filter Tare Wt. _____ g
Difference <u>0.0681</u> g	Difference <u>0.1455</u> g	Difference _____ g
Particulate On Filter Weight <u>0.0681</u> g	Particulate On Filter Weight <u>0.1455</u> g	Particulate On Filter Weight _____ g
Transfer "Particulate On Filter Weight" to Box Number 1.	Transfer "Particulate On Filter Weight" to Box Number 2.	Particulate On Filter Weight" to Box Number 3.
Sum particulate weights from each box labeled "1" and record in box labeled "T1."	Sum particulate weights from each box labeled "2" and record in box labeled "T2."	Sum particulate weights from each box labeled "3" and record in box labeled "T3."
AF 1 <u>0.0681</u> g	AF 2 <u>0.1455</u> g	AF 3 _____ g
Total T1 <u>0.134</u> g	Total T2 <u>0.2347</u> g	Total T3 _____ g

EPA Method 5 Particulate Gravimetric Sheet

Inorganic Residuals

Project LOUISIANA PACIFIC Analyst KAB
 Sampling Location DRYERS OUT Analysis Date(s) 6/17, 6/18, 6/20, 6/21
 Sampling Date 6/15/94 Sampling Reagent _____
 Test Number T1, T2 LDMS Entry _____ Initials _____
 Project Number 940617.500 LDMS Validation 6.22.94 Initials pm

Sample No. 13081.8
 Run Number T1R2
 Dish Number BL

Date/Time 6/21/94 0830
 Gross Weight 108.7677 g

Date/Time 6/21/94 1445
 Gross Weight 108.7676 g

Avg. Gross Wt. 108.7676 g
 Dish Tare Wt. 108.6735 g
 Difference 0.0941 g

Blank Weight 0.0007 g

Inorganic Residuals Wt. 0.0934 g

Transfer "Inorganic Residuals Wt." to Box Number 1.

WC 1 0.0934 g

Sample No. 6/21 13082.6
 Run Number T2R1
 Dish Number LMB

Date/Time 6/21/94 0830
 Gross Weight 107.9778 g

Date/Time 6/21/94 1445
 Gross Weight 107.9778 g

Avg. Gross Wt. 107.9778 g
 Dish Tare Wt. 107.9071 g
 Difference 0.0707 g

Blank Weight 0.0007 g

Inorganic Residuals Wt. 0.0700 g

Transfer "Inorganic Residuals Wt." to Box Number 2.

WC 2 0.0700 g

Sample No. 13083.4
 Run Number T2R2
 Dish Number B5

Date/Time 6/21/94 0830
 Gross Weight 97.5205 g

Date/Time 6/21/94 1445
 Gross Weight 97.5209 g

Avg. Gross Wt. 97.5207 g
 Dish Tare Wt. 97.4119 g
 Difference 0.1088 g

Blank Weight 0.0007 g

Inorganic Residuals Wt. 0.1081 g

Transfer "Inorganic Residuals Wt." to Box Number 3.

WC 3 0.1081 g

EPA Method 5 Particulate Gravimetric Sheet

Organic Condensibles

Project LOUISIANA PACIFIC Analyst KAB
 Sampling Location DRYERS OUT Analysis Date(s) 6/17, 6/18, 6/20, 6/21/94
 Sampling Date 6/15/94 Sampling Reagent _____
 Test Number T172 LDMS Entry _____ Initials _____
 Project Number 940617.500 LDMS Validation C-21-94 Initials gme

Sample No. <u>13081.8</u>	Sample No. <u>13082.6</u>	Sample No. <u>13083.4</u>
Run Number <u>T1R2</u>	Run Number <u>T2R1</u>	Run Number <u>T2R2</u>
Dish Number <u>Z5</u>	Dish Number <u>T</u>	Dish Number <u>87</u>
Date/Time <u>6/21/94 0830</u>	Date/Time <u>6/21/94 0830</u>	Date/Time <u>6/21/94 0830</u>
Gross Weight <u>100.1456</u> g	Gross Weight <u>115.2418</u> g	Gross Weight <u>111.2574</u> g
Date/Time <u>6/21/94 1445</u>	Date/Time <u>6/21/94 1445</u>	Date/Time <u>6/21/94 1445</u>
Gross Weight <u>100.1452</u> g	Gross Weight <u>115.2414</u> g	Gross Weight <u>111.2573</u> g
Avg. Gross Wt. <u>100.1454</u> g	Avg. Gross Wt. <u>115.2416</u> g	Avg. Gross Wt. <u>111.2574</u> g
Dish Tare Wt. <u>100.1096</u> g	Dish Tare Wt. <u>115.1991</u> g	Dish Tare Wt. <u>111.2090</u> g
Difference <u>0.0358</u> g	Difference <u>0.0425</u> g	Difference <u>0.0484</u> g
Blank Weight <u>0.0002</u> g	Blank Weight <u>0.0002</u> g	Blank Weight <u>0.0002</u> g
Condensible Organic Wt. <u>0.0356</u> g	Condensible Organic Wt. <u>0.0423</u> g	Condensible Organic Wt. <u>0.0482</u> g
Transfer "Condensible Organic Wt." to Box Number 1.	Transfer "Condensible Organic Wt." to Box Number 2.	Transfer "Condensible Organic Wt." to Box Number 3.
WC 1 <u>0.0356</u> g	WC 2 <u>0.0423</u> g	WC 3 <u>0.0482</u> g

EPA Method 5 Particulate Gravimetric Sheet

Particulate In Probe Wash

Project LOUISIANA PACIFIC Analyst KAC
 Sampling Location DRYERS OUT Analysis Date(s) 6/17, 6/18, 6/20
 Sampling Date 6/18/94 Cleanup Reagent(s) _____
 Test Number T1, T2 LDMS Entry _____ Initials _____
 Project Number 940617.500 LDMS Validation 6.22-94 Initials ame

Sample No. <u>13081.8</u>	Sample No. <u>13082.6</u>	Sample No. <u>13083.0</u>
Run Number <u>T1R2</u>	Run Number <u>T2R1</u>	Run Number <u>T2R2</u>
Dish Number <u>JJL</u>	Dish Number <u>TD3</u>	Dish Number <u>DDN</u>
Reagent Vol. <u>10</u> ml	Reagent Vol. <u>175</u> ml	Reagent Vol. <u>175</u> ml
Date/Time <u>6/18/94 1600</u>	Date/Time <u>6/18/94 1600</u>	Date/Time <u>6/18/94 1600</u>
Gross Weight <u>97.9438</u> g	Gross Weight <u>97.1128</u> g	Gross Weight <u>102.4689</u> g
Date/Time <u>6/20/94 0830</u>	Date/Time <u>6/20/94 0830</u>	Date/Time <u>6/20/94 0830</u>
Gross Weight <u>97.9436</u> g	Gross Weight <u>97.1123</u> g	Gross Weight <u>102.4693</u> g
Avg. Gross Wt. <u>97.9437</u> g	Avg. Gross Wt. <u>97.1126</u> g	Avg. Gross Wt. <u>102.4691</u> g
Dish Tare Wt. <u>97.9351</u> g	Dish Tare Wt. <u>97.0484</u> g	Dish Tare Wt. <u>102.3464</u> g
Difference <u>0.0086</u> g	Difference <u>0.0642</u> g	Difference <u>0.1227</u> g
Blank Weight <u>0.001</u> g	Blank Weight <u>0.001</u> g	Blank Weight <u>0.001</u> g
Particulate In Rinse Weight <u>0.0076</u> ^{KAC} <u>0.0085</u> _{6/20/94} g	Particulate In Rinse Weight <u>0.0632</u> g	Particulate In Rinse Weight <u>0.1217</u> g
Transfer "Particulate In Rinse Weight" to Box Number 1.	Transfer "Particulate In Rinse Weight" to Box Number 2.	Transfer "Particulate In Rinse Weight" to Box Number 3.
PW 1 <u>0.0076</u> g	PW 2 <u>0.0632</u> g	PW 3 <u>0.1217</u> g

EPA Method 5 Particulate Gravimetric Sheet

Particulate On Filter

Project LOUISIANA PACIFIC Analyst KAB
 Sampling Location DRYERS OUT Analysis Date(s) 6/17/94
 Sampling Date 6/15/94 Filter Type FIBERGLASS, METAL THIMBEL
 Test Number T1, T2 LDMS Entry _____ Initials _____
 Project Number 940617.800 LDMS Validation 6.2294 Initials me

Sample No. <u>13081.8</u>	Sample No. <u>13082.6</u>	Sample No. <u>13083.4</u>
Run Number <u>T1R2</u>	Run Number <u>T2R1</u>	Run Number <u>T2R2</u>
Filter Number <u>#5</u>	Filter Number <u>3084</u>	Filter Number <u>3215</u>
Date/Time <u>6/17/94 1630</u>	Date/Time <u>6/17/94 1630</u>	Date/Time <u>6/17/94 1630</u>
Gross Weight <u>42.3256</u> g	Gross Weight <u>0.8998</u> g	Gross Weight <u>1.0650</u> g
Date/Time _____	Date/Time _____	Date/Time _____
Gross Weight _____ g	Gross Weight _____ g	Gross Weight _____ g
Avg. Gross Wt. <u>42.3256</u> g	Avg. Gross Wt. <u>0.8998</u> g	Avg. Gross Wt. <u>1.0650</u> g
Filter Tare Wt. <u>42.1703</u> g	Filter Tare Wt. <u>0.67375</u> g	Filter Tare Wt. <u>0.66579</u> g
Difference <u>0.1553</u> g	Difference <u>0.2260</u> g	Difference <u>0.3992</u> g
Particulate On Filter Weight <u>0.1553</u> g	Particulate On Filter Weight <u>0.2260</u> g	Particulate On Filter Weight <u>0.3992</u> g
Transfer "Particulate On Filter Weight" to Box Number 1.	Transfer "Particulate On Filter Weight" to Box Number 2.	Particulate On Filter Weight" to Box Number 3.
Sum particulate weights from each box labeled "1" and record in box labeled "T1."	Sum particulate weights from each box labeled "2" and record in box labeled "T2."	Sum particulate weights from each box labeled "3" and record in box labeled "T3."
AF 1 <u>0.1553</u> g	AF 2 <u>0.2260</u> g	AF 3 <u>0.3992</u> g
Total T1 <u>0.2919</u> g	Total T2 <u>0.4015</u> g	Total T3 <u>0.6697</u> g
		<u>0.6772</u> g



REPORT OF LABORATORY ANALYSIS

Louisiana Pacific
Route 8, Box 8030
Hayward, WI 54843

June 27, 1994
PACE Project Number: 940617500

Attn: Ms. Susan Somers

Client Reference: L.P. Hayward

PACE Sample Number:

Date Collected:

Date Received:

Client Sample ID:

10 0130770 10 0130788 10 0130796

06/15/94 06/15/94 06/15/94

06/17/94 06/17/94 06/17/94

Line 2 Line 1 Line 2 EFB

Core Dryer Core Dryer Core Dryer

Parameter

Units

MDI

Out. TIR1 Out. TIR2 Out. TIR1

INORGANIC ANALYSIS

EPA 5: TOTAL PARTICULATE EMISSIONS

Particulates, filter	g	0.0001	0.3924	0.2065	0.1335
Particulates, probe wash	g	0.0001	0.0809	0.0595	0.0061
Particulates, Inorganic Residuals	g	0.0001	0.1067	0.0600	0.0567
Particulates, Organic Condensibles	g	0.0001	0.0479	0.0271	0.0256
Particulates, total-EPA 5	g	0.0001	0.6279	0.3531	0.2239

REPORT OF LABORATORY ANALYSIS

Ms. Susan Somers
Page 2

June 27, 1994
PACE Project Number: 940617500

Client Reference: L.P. Hayward

PACE Sample Number:

10 0130818 10 0130826 10 0130834

Date Collected:

06/15/94 06/15/94 06/15/94

Date Received:

06/17/94 06/17/94 06/17/94

Client Sample ID:

Line 1 EFB Line 2 Line 1

Parameter

Units

MDI

Core Dryer Surf Dryer Surf Dryer
Out. T1R2 Out. T2R1 Out. T2R2

INORGANIC ANALYSIS

EPA 5: TOTAL PARTICULATE EMISSIONS

Particulates, filter	g	0.0001	0.1553	0.226	0.3992
Particulates, probe wash	g	0.0001	0.0076	0.0632	0.1217
Particulates, Inorganic Residuals	g	0.0001	0.0934	0.07	0.1081
Particulates, Organic Condensibles	g	0.0001	0.0356	0.0423	0.0482
Particulates, total-EPA 5	g	0.0001	0.2919	0.4015	0.6772

REPORT OF LABORATORY ANALYSIS

Ms. Susan Somers
Page 3

June 27, 1994
PACE Project Number: 940617500

Client Reference: L.P. Hayward

PACE Sample Number:	10 0130850	10 0130869
Date Collected:	06/15/94	06/15/94
Date Received:	06/17/94	06/17/94
Client Sample ID:	Line 2 EFB	Line 1 EFB
	Surf Dryer	Surf Dryer
Parameter	Units	MDI
	Out. T2R1	Out. T2R2

INORGANIC ANALYSIS

EPA 5: TOTAL PARTICULATE EMISSIONS

Particulates, filter	g	0.0001	0.0681	0.1455
Particulates, probe wash	g	0.0001	0.0057	0.0069
Particulates, Inorganic Residuals	g	0.0001	0.0457	0.0739
Particulates, Organic Condensibles	g	0.0001	0.0145	0.0280
Particulates, total-EPA 5	g	0.0001	0.134	0.2543

These data have been reviewed and are approved for release.

Mary Jo Connolly
Project Manager

REPORT OF LABORATORY ANALYSIS

Ms. Susan Somers
Page 4

FOOTNOTES
for pages 1 through 3

June 27, 1994
PACE Project Number: 940617500

Client Reference: L.P. Hayward

MDL Method Detection Limit

APPENDIX C
Calculation Equations and Report Nomenclature

Louisiana - Pacific Corporation
Hayward, Wisconsin
PACE Project No. 940614.401

PACE Incorporated
June 22, 1994

APPENDIX C
METHOD 5 CALCULATION SUMMARY

Line No. 1 EFB Outlet

Parameter	Run 2	Run 2
Date of Run	6/16/94	6/16/94
Sample Duration (Minutes)	60	60
Barometric Pressure (inches Hg)	28.63	28.63
Static Pressure Of Duct (Inches H2O)	6	6
Absolute Pressure Of Duct (Inches Hg)	29.07	29.07
Meter Coefficient	1.0044	1.0044
Pitot Tube Coefficient	0.843	0.843
Nozzle Diameter (Inches)	0.235	0.235
Area Of Nozzle Opening (Square Feet)	0.000301	0.000301
Average $\sqrt{\Delta P}$	0.9886	0.9740
Average ΔH	1.55	1.52
Average Stack Temperature (°R)	702.00	694.83
Average Meter Temperature (°R)	552.08	538.96
Meter Volume (Cubic Feet)	45.12	44.16
Dry Standard Sample Volume (Cubic Feet)	41.64	41.74
Collected Condensate Volume (mls)	323.0	306.0
Volume Of Water Vapor (Standard Cubic Feet)	15.20	14.40
Moisture Content Of Flue Gas (% v/v)	26.75	25.65
Weight Of Particulate (mg)	291.9	254.3
Particulate Concentration (GR/DSCF)	0.10818627	0.09401762
Source Gas Velocity (Feet Per Second)	68.3	66.8
Isokinetic Variation (%)	105.1	105.1

Louisiana - Pacific Corporation
Hayward, Wisconsin
PACE Project No. 940614.401

PACE Incorporated
June 22, 1994

APPENDIX C
METHOD 5 CALCULATION SUMMARY

Line No. 1 Dryers

Parameter	Core Dryer	Surface Dryer
Date of Run	6/16/94	6/16/94
Sample Duration (Minutes)	54	60
Barometric Pressure (inches Hg)	28.63	28.63
Static Pressure Of Duct (Inches H2O)	-8.2	-9
Absolute Pressure Of Duct (Inches Hg)	28.03	27.97
Meter Coefficient	0.9992	0.9992
Pitot Tube Coefficient	0.835	0.835
Nozzle Diameter (Inches)	0.198	0.198
Area Of Nozzle Opening (Square Feet)	0.000214	0.000214
Average $\sqrt{\Delta P}$	1.1578	1.2121
Average ΔH	0.95	1.09
Average Stack Temperature (°R)	705.89	707.35
Average Meter Temperature (°R)	554.03	534.80
Meter Volume (Cubic Feet)	29.65	36.66
Dry Standard Sample Volume (Cubic Feet)	27.08	34.70
Collected Condensate Volume (mls)	160.0	312.0
Volume Of Water Vapor (Standard Cubic Feet)	7.53	14.69
Moisture Content Of Flue Gas (% v/v)	21.76	29.74
Weight Of Particulate (mg)	353.1	677.2
Particulate Concentration (GR/DSCF)	0.20119692	0.30114642
Source Gas Velocity (Feet Per Second)	80.1	85.4
Isokinetic Variation (%)	89.1	107.7

Louisiana - Pacific Corporation
Hayward, Wisconsin
PACE Project No. 940614.401

PACE Incorporated
June 22, 1994

APPENDIX C
METHOD 5 CALCULATION SUMMARY

Line No. 2 EFB Outlet

Parameter	Run 1	Run 1
Date of Run	6/16/94	6/16/94
Sample Duration (Minutes)	60	39
Barometric Pressure (inches Hg)	28.63	28.63
Static Pressure Of Duct (Inches H2O)	-5	-5
Absolute Pressure Of Duct (Inches Hg)	28.26	28.26
Meter Coefficient	0.9942	0.9942
Pitot Tube Coefficient	0.843	0.843
Nozzle Diameter (Inches)	0.239	0.239
Area Of Nozzle Opening (Square Feet)	0.000312	0.000312
Average $\sqrt{\Delta P}$	1.0735	1.1095
Average ΔH	1.96	2.09
Average Stack Temperature (°R)	680.75	682.00
Average Meter Temperature (°R)	553.46	551.44
Meter Volume (Cubic Feet)	50.34	33.76
Dry Standard Sample Volume (Cubic Feet)	45.92	30.92
Collected Condensate Volume (mls)	284.0	182.0
Volume Of Water Vapor (Standard Cubic Feet)	13.37	8.57
Moisture Content Of Flue Gas (% v/v)	22.55	21.70
Weight Of Particulate (mg)	221.9	134.0
Particulate Concentration (GR/DSCF)	0.07457647	0.06688604
Source Gas Velocity (Feet Per Second)	73.6	75.9
Isokinetic Variation (%)	98.1	97.6

Louisiana - Pacific Corporation
Hayward, Wisconsin
PACE Project No. 940614.401

PACE Incorporated
June 22, 1994

APPENDIX C
METHOD 5 CALCULATION SUMMARY

Line No. 2 Dryers

Parameter	Core Dryer Outlet	Surface Outlet
Date of Run	6/16/94	6/16/94
Sample Duration (Minutes)	60	36
Barometric Pressure (inches Hg)	28.63	28.63
Static Pressure Of Duct (Inches H2O)	-16	-14.2
Absolute Pressure Of Duct (Inches Hg)	27.45	27.59
Meter Coefficient	1.0044	1.0044
Pitot Tube Coefficient	0.835	0.835
Nozzle Diameter (Inches)	0.2	0.2
Area Of Nozzle Opening (Square Feet)	0.000218	0.000218
Average $\sqrt{\Delta P}$	1.3010	1.4328
Average ΔH	1.36	1.76
Average Stack Temperature (°R)	679.58	677.67
Average Meter Temperature (°R)	562.96	564.25
Meter Volume (Cubic Feet)	43.15	28.89
Dry Standard Sample Volume (Cubic Feet)	39.03	26.10
Collected Condensate Volume (mls)	185.0	161.0
Volume Of Water Vapor (Standard Cubic Feet)	8.71	7.58
Moisture Content Of Flue Gas (% v/v)	18.24	22.50
Weight Of Particulate (mg)	627.9	401.5
Particulate Concentration (GR/DSCF)	0.24825483	0.23739543
Source Gas Velocity (Feet Per Second)	88.6	98.1
Isokinetic Variation (%)	96.3	101.4

Calculation Equations

Nomenclature

A	= Cross-sectional area of duct
A_n	= Cross-sectional area of nozzle
B_{ws}	= Water vapor in gas stream, proportion by volume
C_a	= Particulate concentration, actual, wet basis - GR/ACF
C_p	= Pitot tube calibration coefficient
C_s	= Particulate concentration at dry standard conditions - GR/DSCF
%EA	= Excess air, percent by volume
F_o	= Fuel factor
G_d	= Specific gravity relative to air, dimensionless
I	= Isokinetic variation, percent by volume
M_d	= Molecular weight of flue gas, dry, lb/lb-mole
m_g	= Mass flow of wet flue gas, LB/HR
m_n	= Total particulate collected, grams
m_p	= Particulate mass flow, LB/HR
M_s	= Molecular weight of flue gas, wet, lb/lb-mole
P_b	= Barometric pressure, uncompensated, inches of mercury
P_g	= Static pressure of duct, inches of water
P_s	= Absolute gas pressure of duct, inches of mercury
Q	= Actual flue gas volumetric flow rate, ACFM
Q_{sd}	= Dry flue gas volumetric flow rate corrected to standard conditions, DSCFM
$\overline{T_m}$	= Average dry gas meter temperature, °R
$\overline{T_s}$	= Average stack gas temperature, °R
$\emptyset$	= Total sampling time, minutes
V_{lc}	= Total volume of liquid collected in impingers and desiccant, ml
V_m	= Volume of gas sample measured by gas meter, cubic feet
V_{std}	= Volume of gas sample corrected to standard conditions, dry standard cubic feet
V_w	= Volume of water vapor in gas sample, corrected to standard conditions
V_s	= Linear velocity of flue gas, feet per second
Y	= Dry gas meter calibration factor
ΔH	= Orifice meter differential pressure, inches of water
ΔP	= Velocity pressure of flue gas, inches of water
B	= Actual gas density, pounds per cubic foot

Calculation Equations

EPA Method 2 Calculations

Flue Gas Linear Velocity

$$V_s = 85.49 \times C_p \times \sqrt{\Delta P} \times \sqrt{\frac{T_s}{P_s \times M_s}}$$

Volumetric Flow Rates - ACFM, SCFM & DSCFM

$$Q = 60 \times v_s \times A$$

$$Q_s = Q \times \left(\frac{528}{T_s} \right) \times \left(\frac{P_s}{29.92} \right) = Q \times 17.647 \times \left(\frac{P_s}{T_s} \right)$$

$$Q_{sd} = Q_s \times (1 - B_{ws})$$

Mass Flow Rate of Wet Flue Gas

$$m_g = \frac{4.995 \times Q_{sd} \times G_d}{1 - B_{ws}}$$

Actual Gas Density

$$\rho = \frac{0.04585 \times P_s \times M_s}{T_s}$$

Where:

- A = Cross-sectional area of duct at sample point (sq. ft.).
- B_{ws} = Water vapor in gas stream (proportion by volume).
- C_p = Pitot tube calibration coefficient.
- G_d = Flue gas specific gravity relative to air, dimensionless.
- m_g = Mass flow rate of wet flue gas (LB/HR).
- M_s = Molecular weight of wet flue gas (LB/LB-mole).
- P_s = Absolute gas pressure of duct (Inches Hg).
- ΔP = Velocity pressure measured by pitot tube (Inches WC).
- Q = Actual flue gas volumetric flow rate (ACFM).
- Q_s = Volumetric gas flow at standard conditions (SCFM).
- Q_{sd} = Dry standard volumetric gas flow rate (DSCFM).
- T_s = Flue gas temperature (°R).
- V_s = Flue gas linear velocity (feet per second).
- ρ = Actual flue gas density (LB/CF).

Calculation Equations

EPA Method 3 Calculations

Dry Molecular Weight of Flue Gas

$$M_d = (0.44 \times \%CO_2) + (0.32 \times \%O_2) + (0.28 \times (\%N_2 + \%CO))$$

Wet Molecular Weight of Flue Gas

$$M_s = M_d \times (1 - B_{ws}) + (18 \times B_{ws})$$

Percent Excess Air

$$\%EA = 100 \times \left(\frac{\%O_2 - (0.05 \times \%CO)}{(0.264 \times \%N_2) - \%O_2 + (0.5 \times \%CO)} \right)$$

Fuel F-factor (for comparison)

$$F_o = \frac{20.9 - \%O_2}{\%CO_2}$$

Where:

- B_{ws} = Water vapor in gas stream (proportion by volume).
- $\%CO$ = Carbon monoxide in gas stream (percent).
- $\%CO_2$ = Carbon dioxide in gas stream (percent).
- $\%EA$ = Excess air for combustion (percent).
- F_o = Fuel F-factor for results comparison.
- M_d = Molecular weight of dry flue gas (LB/LB-mole).
- M_s = Molecular weight of wet flue gas (LB/LB-mole).
- $\%N_2$ = Nitrogen in gas stream (percent).
- $\%O_2$ = Oxygen in gas stream (percent).

Calculation Equations

EPA Method 4 Calculations

Sample Volume, Standard Conditions

$$V_{std} = 17.647 \times V_m \times Y \times \left(\frac{P_b + \frac{\Delta H}{13.6}}{T_m} \right)$$

Volume of Water Vapor Sampled

$$V_w = 0.047070 \times V_{lc}$$

Proportion of Water Vapor in Sampled Gas

$$B_{ws} = \frac{V_w}{V_w + V_{std}}$$

Where:

- B_{ws} = Water vapor in gas stream (proportion by volume).
- ΔH = Orifice meter differential pressure (Inches WC).
- P_b = Barometric pressure (Inches Hg).
- T_m = Sampling train meter temperature ($^{\circ}R$).
- V_{lc} = Total volume of liquid collected in sampling train (mls).
- V_m = Volume of gas sample measured by gas meter (CF).
- V_{std} = Gas volume corrected to standard conditions (DSCF).
- V_w = Volume of water vapor in gas sample (SCF).
- Y = Dry gas meter calibration coefficient.

Calculation Equations

EPA Method 5 Calculations

Sample Volume, Standard Conditions

$$V_{std} = 17.647 \times V_m \times Y \times \left(\frac{P_b + \frac{\overline{\Delta H}}{13.6}}{\overline{T}_m} \right)$$

Isokinetic Variation

$$I = 0.09450 \times \left(\frac{\overline{T}_s \times V_m}{P_s \times V_s \times A_n \times \theta \times (1 - B_{ws})} \right)$$

Particulate Concentration

$$C_s = 15.432 \times \left(\frac{m_n}{V_{std}} \right)$$

Particulate Mass Rate

$$m_p = 0.008571 \times C_s \times Q_{sd}$$

Where:

- A_n = Cross-sectional area of nozzle opening (square feet).
- B_{ws} = Water vapor in gas stream (proportion by volume).
- C_s = Particulate concentration of gas stream (GR/DSCF).
- ΔH = Orifice meter differential pressure (Inches WC).
- I = Isokinetic variation of sampling rate (percent).
- m_n = Total particulate collected in sampling train (grams).
- m_p = Particulate mass flow rate (LB/HR).
- P_b = Barometric pressure (Inches Hg).
- P_s = Absolute gas pressure of duct (Inches Hg).
- Q_{sd} = Dry standard volumetric gas flow rate (DSCFM).
- $\overline{T}_m$ = Sampling train meter temperature ($^{\circ}$ R).
- $\overline{T}_s$ = Flue gas temperature ($^{\circ}$ R).
- V_m = Volume of gas sample measured by gas meter (CF).
- V_{std} = Gas volume corrected to standard conditions (DSCF).
- V_s = Flue gas linear velocity (feet per second).
- Y = Dry gas meter calibration coefficient.
- θ = Total sampling time of run (minutes).

APPENDIX D
Test Procedures

OXYGEN AND CARBON DIOXIDE CONCENTRATION (ORSAT)

Integrated gas samples are collected in 40 liter Tedlar™ bags and ultimately transferred to an Orsat gas analyzer for oxygen and carbon dioxide analyses. A PACE sampling train which meets or exceeds the specifications of EPA Method 3, 40 CFR 60, Appendix A is used to collect gas samples. Normally, gas samples are collected at the exhaust of an EPA Method 4 or 5 sampling train since this gas stream is moisture conditioned. Method 4 and 5 sampling equipment is maintained and checked to assure no leaks occur between the flue and the integrated gas sampler.

Gas samples are collected by drawing a portion of the stream through a chemically resistant diaphragm pump and delivering it to the Tedlar™ bag at a constant, settable rate depending on expected sampling time. At the conclusion of sampling, the bag and associated hardware is sealed and labeled. When multiple tests are to be performed, gas samples are often transferred to glass gas collection tubes for storage. A portable oxygen analyzer is used for this to ensure sample integrity.

Samples are analyzed by chemical absorption using an Orsat gas analyzer. Following positive and negative leak checks of the gas analyzer, the system is purged with the gas to be analyzed. The buret is filled with approximately 100 mls of sample gas and the exact volume recorded. The sample line stopcock is closed and the stopcock for the first bubbler containing carbon dioxide absorbent is opened. Several passes are made, bubbling the sample gas through the reagent and the absorbent is returned to the initial mark. The new volume of the buret is recorded and an additional 1-2 passes are made to verify total absorption. Similar procedures are used to quantify oxygen with the same gas aliquot and oxygen absorbent.

PARTICULATE LOADINGS AND EMISSION RATES

Particulate emission rates were determined in accordance with EPA Methods 1-5, 40 CFR 60, Appendix A. Using traverse points determined with EPA Method 1, a preliminary velocity profile was obtained with respect to the velocity traverse, gas temperature, gas pressure and estimated moisture content. From this data sampling nozzles of the appropriate diameter to ensure isokinetic sampling were selected.

The particulate sampling train consists of a temperature controlled glass lined sampling probe equipped with a S-type pitot tube and Type K thermocouples to monitor stack temperature and probe liner temperature. The sampling probe is attached to a sample module which houses an all glass in-line filter and cyclone assembly in a temperature controlled oven. The back half of the sampling train consists of a series of three glass impingers followed by a tared desiccant-packed drying column. The sample train is connected by means of a control and sampling umbilical cord to the control module. The control module houses a temperature monitored dry test gas meter, a calibrated orifice, dual inclined manometers, temperature controllers, and necessary flow rate control devices.

Particulate samples are collected by isokinetically extracting a sample gas stream from the flue by means of the sampling probe and passing the stream through the cyclone which collects larger, heavier particles. The sample gas stream then passes through a 4 inch diameter Gelman Type A/E glass fiber filter to collect finer particulates. The filter is followed by an ice-cooled impinger train and a desiccant packed drying column which quantitatively collects all moisture from the sample gas stream. The gas then passes through a leak proof rotary vane sampling pump and a dry test gas meter which integrates the sample volume throughout the course of the test. A calibrated orifice is connected to the gas meter outlet to facilitate sample flow rate adjustment.

Representative particulate samples are collected by sampling the centroid of equal area sections of the duct for equal time periods. The sampling rate is adjusted at each traverse point to ensure isokinetic sampling. Pre-programmed

field computers are used to facilitate rapid determination of the correct sampling rate.

Integrated gas samples are collected concurrently with particulate samples to determine a representative gas composition of the flue gas. Gas samples are collected in Tedlar™ bags throughout the course of the particulate run and analyzed with an Orsat gas analyzer.

At the end of each particulate run, the sampling train is disassembled and the samples recovered. The sampling filter is transferred from the filter holder to its dedicated petri dish. The probe nozzle is acetone rinsed, brushed, rinsed again and the washings placed in a uniquely labeled polyethylene container. The probe is similarly cleaned; acetone rinsed, brushed several times, rinsed again and the washing transferred to the same polyethylene container. The filter holder and cyclone are wiped free of silicone grease, acetone rinsed, brushed, rinsed and these washings added to the probe wash container. The container is tightly capped and the liquid level marked for transport. The impinger catch volume is determined to the nearest milliliter using a graduated cylinder. If the impinger catch is to be analyzed it is transferred to a separate polyethylene container, capped, and the liquid level marked. The desiccant-packed drying column is weighed in the field to the nearest 0.5 g and the weight of absorbed moisture added to the condensate for moisture calculations.

Particulate samples are transported back to the laboratory, logged in, and prepared for analyses. Filters are desiccated for 24 hours and weighed to a constant weight and the results recorded to the nearest 0.1 mg. Probe wash samples are evaporated at ambient temperatures to dryness in tared evaporating dishes. They are then desiccated for 24 hours and weighed to a constant weight. Results are reported to the nearest 0.1 mg.

WET CATCH ANALYSIS - ORGANIC CONDENSIBLES

Particulate concentrations reported in this document include gravimetric results of both the dry catch and the organic wet catch. Organic condensibles were collected in a series of three ice-cooled all-glass impingers in the back half of the Method 5 sampling train. The first two impingers were initially prepared with 100 mls of deionized water in each and the third impinger was dry. After sampling, the volume of condensate in the impingers was determined and the contents transferred to an air-tight polyethylene sample container.

The wet catch was analyzed for condensible organic particulate with the chloroform/diethyl ether extraction. Three 25 ml portions of chloroform and three 25 ml portions of diethyl ether were used to extract condensed organics from the impinger catches (wet catch). The extractions were evaporated at room temperature and desiccated to a constant weight. Gravimetric results were then added to dry catch results to calculate particulate concentrations.

WET CATCH ANALYSES - INORGANIC RESIDUE

Particulate concentrations reported in this document include gravimetric results of both the dry catch and the wet catch. A series of three ice-cooled all-glass impingers was used in the back half of the Method 5 train to collect moisture, dissolved solids and extremely fine particulates. Each of the first two impingers were initially prepared with 100 mls of deionized distilled water and the third impinger was dry. After sampling, the volume of condensate in the impingers was determined and the contents transferred to an air-tight polyethylene container.

The wet catch samples were analyzed by evaporating in a tared beaker at a temperature less than 180 °F. After samples were evaporated to dryness, they were desiccated for 24 hours then weighed to a constant weight. Gravimetric results were then added to dry catch results to calculate particulate concentrations.

APPENDIX E
Quality Assurance Data

SAMPLING TRAIN CALIBRATION DATA

Louisiana-Pacific Corporation
Hayward, Wisconsin
PACE Project No. 940614.401

PACE Incorporated
July 14, 1994

Air Sampling Department Calibration Report

Sampling Nozzle Calibration Data

Nozzle Number : 3-1
Date of Calibration : 5/20/94
Calibration Technician: M. Wilson

Measurement Position	Diameter Inches
1	0.201
2	0.199
3	0.198
4	0.201
5	0.199
Average	0.200

The sampling nozzle is rotated and measured at 36 degree
increments. Diameters are measured to the nearest 0.001".
All measurements must be within a range of 0.004".

Louisiana-Pacific Corporation
Hayward, Wisconsin
PACE Project No. 940614.401

PACE Incorporated
July 14, 1994

Air Sampling Department Calibration Report

Sampling Nozzle Calibration Data

Nozzle Number : 3-2
Date of Calibration : 5/20/94
Calibration Technician: M. Wilson

Measurement Position	Diameter Inches
1	0.238
2	0.240
3	0.239
4	0.239
5	0.238
Average	0.239

The sampling nozzle is rotated and measured at 36 degree increments. Diameters are measured to the nearest 0.001". All measurements must be within a range of 0.004".

Louisiana-Pacific Corporation
Hayward, Wisconsin
PACE Project No. 940614.401

PACE Incorporated
July 14, 1994

Air Sampling Department Calibration Report

Sampling Nozzle Calibration Data

Nozzle Number : 4-1
Date of Calibration : 5/20/94
Calibration Technician: M. Wilson

Measurement Position	Diameter Inches
1	0.197
2	0.199
3	0.199
4	0.198
5	0.197
Average	0.198

The sampling nozzle is rotated and measured at 36 degree increments. Diameters are measured to the nearest 0.001". All measurements must be within a range of 0.004".

Louisiana-Pacific Corporation
Hayward, Wisconsin
PACE Project No. 940614.401

PACE Incorporated
July 14, 1994

Air Sampling Department Calibration Report

Pitot Tube Calibration Data

Pitot Tube Number : 2
Date of Calibration : 7/7/93
Calibration Technician: K. Lattery

A Side Calibration

Calibration Trial No.	ΔP (standard) Inches WC	ΔP (S-type) Inches WC	Pitot Coefficient
1	0.505	0.715	0.832
2	0.795	1.120	0.834
3	1.100	1.530	0.839
4	1.290	1.820	0.833
A Side Average			0.835

B Side Calibration

Calibration Trial No.	ΔP (standard) Inches WC	ΔP (S-type) Inches WC	Pitot Coefficient
1	0.500	0.705	0.834
2	0.790	1.115	0.833
3	1.120	1.560	0.839
4	1.295	1.830	0.833
B Side Average			0.835
Pitot Tube Coefficient			0.835

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Hayward, Wisconsin
PACE Project No. 940614.401

PACE Incorporated
July 14, 1994

Air Sampling Department Calibration Report

Pitot Tube Calibration Data

Pitot Tube Number : 24
Date of Calibration : 6/8/93
Calibration Technician: K. Lattery

A Side Calibration

Calibration Trial No.	ΔP (standard) Inches WC	ΔP (S-type) Inches WC	Pitot Coefficient
1	0.480	0.675	0.835
2	0.800	1.095	0.846
3	1.135	1.560	0.844
4	1.325	1.850	0.838
A Side Average			0.841

B Side Calibration

Calibration Trial No.	ΔP (standard) Inches WC	ΔP (S-type) Inches WC	Pitot Coefficient
1	0.490	0.675	0.843
2	0.795	1.085	0.847
3	1.110	1.540	0.840
4	1.345	1.840	0.846
B Side Average			0.844
Pitot Tube Coefficient			0.843

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July 14, 1994

Air Sampling Department Calibration Report

Pitot Tube Calibration Data

Pitot Tube Number : 8
Date of Calibration : 3/19/94
Calibration Technician: M. McDermott

A Side Calibration

Calibration Trial No.	ΔP (standard) Inches WC	ΔP (S-type) Inches WC	Pitot Coefficient
1	0.485	0.665	0.845
2	0.800	1.105	0.842
3	1.095	1.510	0.843
4	1.300	1.800	0.841
A Side Average			0.843

B Side Calibration

Calibration Trial No.	ΔP (standard) Inches WC	ΔP (S-type) Inches WC	Pitot Coefficient
1	0.490	0.680	0.840
2	0.800	1.110	0.840
3	1.100	1.525	0.841
4	1.305	1.810	0.841
B Side Average			0.841
Pitot Tube Coefficient			0.842

Louisiana-Pacific Corporation
 Hayward, Wisconsin
 PACE Project No. 940614.401

PACE Incorporated
 July 14, 1994

Air Sampling Section Calibration Report

Dry Test Meter and Orifice Calibration Data

Control Module Number : C-7

Calibration Technician: M.Wilson

Date of Calibration : 5/20/94

Barometric Pressure : 29.00

Orifice Diff. Press., ΔH Inches WC	Dry Test Meter Vol. Cubic Ft.	Wet Test Meter Vol. Cubic Ft.	Dry Test Meter Temperatures, °F		Wet Test Meter Temp., °F	Elapsed Time Minutes	Gas Meter Coefficient $\frac{Q}{Q_0}$	Orifice Coefficient $\Delta H @$
			Inlet	Outlet				
0.50	5.040	5.000	81.0	88.5	74.5	12.156	1.0098	1.683
1.00	5.050	5.000	81.0	88.0	74.5	8.579	1.0061	1.678
1.75	5.080	5.000	81.5	93.5	74.5	6.550	1.0037	1.694
2.50	10.200	10.000	84.0	97.0	74.5	10.947	1.0034	1.680
3.50	10.240	10.000	85.5	97.5	74.5	9.341	0.9988	1.711

Average Meter Coefficient 1.0044

Average Orifice Coefficient 1.689

Louisiana-Pacific Corporation
Hayward, Wisconsin
PACE Project No. 940614.401

PACE Incorporated
July 14, 1994

Air Sampling Section Calibration Report

Dry Test Meter and Orifice Calibration Data

Control Module Number : C-5

Calibration Technician: M. Wilson

Date of Calibration : 5/26/94

Barometric Pressure : 28.95

Orifice Diff. Press., ΔH <u>Inches WC</u>	Dry Test Meter Vol. <u>Cubic Ft.</u>	Wet Test Meter Vol. <u>Cubic Ft.</u>	Dry Test Meter Temperatures, °F		Wet Test Meter Temp., °F	Elapsed Time <u>Minutes</u>	Gas Meter Coefficient <u>$\frac{d}{d}$</u>	Orifice Coefficient <u>$\Delta H @$</u>
			<u>Inlet</u>	<u>Outlet</u>				
0.50	5.090	5.000	80.5	74.0	69.5	12.062	0.9954	1.673
1.00	5.080	5.000	82.5	74.0	69.5	8.655	0.9980	1.723
1.75	5.010	5.000	80.0	70.5	70.0	6.636	1.0034	1.787
2.50	10.080	10.000	84.0	72.0	69.5	11.184	1.0016	1.805
3.50	10.120	10.000	85.0	73.5	69.5	9.481	0.9975	1.810

Average Meter Coefficient 0.9992

Average Orifice Coefficient 1.760