

Note: This is a reference cited in AP 42, *Compilation of Air Pollutant Emission Factors, Volume I Stationary Point and Area Sources*. AP42 is located on the EPA web site at www.epa.gov/ttn/chief/ap42/

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Background Report 4

Reference Number: 84

**Title: Report of Air Emissions and Inlet
Loading Tests for Kirby Forest
Industries, Silsbee OSB Facility
Press House Numbers 1 & 2 Vent
Ducts, Silsbee Texas, April 27, 1995**

**Environmental Monitoring
Laboratories, Inc.**

May 1995

4.84)

REPORT OF
AIR EMISSIONS AND INLET LOADING TESTS
FOR
KIRBY FOREST INDUSTRIES - SILSBEE OSB FACILITY
PRESS VENT RTO

Silsbee, Texas
April 27, 1995

Prepared for
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Subject: Kirby Forest Industries
Silsbee, Texas

On April 27, 1995, Environmental Monitoring Laboratories performed air emissions testing for Kirby Forest Industries' oriented strand board (OSB) facility in Silsbee, Texas. Testing was performed to determine emissions of particulate matter (PM) and total hydrocarbon as carbon (VOC) from the Press Vent regenerative thermal oxidizer (RTO). Testing was also done at the inlet to determine inlet loading of PM and VOC. This testing was done at the request of Louisiana Pacific Corporation. Kirby Forest Industries is a wholly owned subsidiary of Louisiana Pacific Corporation.

Results are shown in the table below.

	PARTICULATE		VOC AS C	
	#/hr	gr/dscf	#/hr	ppm
Outlet	1.87	0.002	3.05	17
Inlet	12.01	0.018	43.03	293
Removal Efficiency	84%	89%	93%	94%

The testing project was coordinated by Dr. James T. Boswell of Louisiana Pacific Corporation. Danny Russell of Environmental Monitoring laboratories coordinated sample collection and analysis and report preparation.

Following is a report of the test.

REPORT OF AIR EMISSIONS AND INLET LOADING TESTS FOR
KIRBY FOREST INDUSTRIES – SILSBEE OSB FACILITY
PRESS VENT RTO
SILSBEE, TEXAS
APRIL 27, 1995

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REPORT CERTIFICATION

I certify that I have examined the information submitted herein,
and based upon my inquiries of those responsible for obtaining the
data or upon my direct acquisition of data, I believe the submitted
information is true, accurate and complete.

Signed 

Daniel G. Russell

1.0 TEST RESULTS: The following tables present the measured flow parameters and test results for air emissions and loading testing done on April 27, 1995, for Kirby Forest Industries 's OSB facility in Silsbee, Texas.

**Kirby Forest Industries -- Silsbee OSB Facility
Press Vent RTO**

Run No.		1	2	3	AVG.
Date		4/27/95	4/27/95	4/27/95	—
Time Start		1150	1402	1542	—
Time End		1251	1502	1642	—
PARTICULATE EMISSIONS	#/hr	1.84	1.96	1.82	1.87
PARTICULATE EMISSIONS	gr/dscf	0.002	0.002	0.002	0.002
VOC EMISSIONS	#/hr	3.07	3.20	2.89	3.05
VOC EMISSIONS	ppm	17.5	16.0	16.5	16.6
VOLUMETRIC FLOWRATE	acfm	135484	155396	136998	142626
VOLUMETRIC FLOWRATE	dscfm	93968	106920	93881	98256
VELOCITY	ft./sec.	52.6	60.3	53.1	55.3
STACK TEMPERATURE	°F	273	276	272	274
MOISTURE	%	3.9	4.3	5.2	4.5
SAMPLE RATE	% isokinetic	95	94	95	95

Kirby Forest Industries - Silsbee, Texas
Press Vents RTO Inlet

Run No.		1	2	3	AVG.
Date		4/27/95	4/27/95	4/27/95	—
Time Start		1845	2015	2004	—
Time End		1948	2118	2108	—
PARTICULATE EMISSIONS	#/hr	24.22	11.26	12.77	12.01
PARTICULATE EMISSIONS	gr/dscf	0.036	0.017	0.019	0.018
VOC EMISSIONS	#/hr	48.03	39.82	41.24	43.03
VOC EMISSIONS	ppm	327.5	275.3	275.0	292.6
VOLUMETRIC FLOWRATE	acfm	109255	108581	113209	110348
VOLUMETRIC FLOWRATE	dscfm	78447	77365	80214	78675
VELOCITY	ft./sec.	68.3	67.9	70.8	69.0
STACK TEMPERATURE	°F	126	129	133	129
MOISTURE	%	3.8	4.1	4.0	4.0
SAMPLE RATE	% isokinetic	90	91	90	90

Run No. 1 particulate results deleted from average

2.0 SOURCE DESCRIPTION: Kirby Forest Industries, a wholly owned subsidiary of Louisiana Pacific Corporation, operates an Oriented Strand Board (OSB) plant in Silsbee, Texas. A Research Cottrell regenerative thermal oxidizer (RTO) has been installed to control emissions from the press vent.

Source description here is limited to a description of the sampling locations. Detailed process descriptions and operating conditions during testing may be supplied by Louisiana Pacific Corporation.

The RTO exhausts to the atmosphere by way of a 88.75 inch diameter vertical stack extending through the roof of the building housing the press. Two sample ports at 90° are provided at a location that is 25 feet (3.3 diameters) below the point where the stack exits the roof and 20 feet (2.7 diameters) above the system inlet duct to stack transition. Sketches of the stack and sampling locations are provided in Appendix A.

The RTO inlet has two ducts from the press. Both inlets were sampled in a rectangular, horizontal section of duct leading to a knock out chamber. Each duct is equipped with four sample ports along the vertical wall of the duct.

3.0 TEST PROCEDURES: Test procedures used are those described in 40 CFR, Part 60, Appendix A and in Part 266, Appendix IX..

Particulate sampling was done as described in Method 5. An exception was the inclusion of the condenser section particulate as described in Method 202. Reported particulate is based on three fractions: the front half, the back half organic (methylene chloride extraction), and the back half aqueous. The contribution of each fraction can be reviewed in Section 4.0.

VOC concentrations were measured using Method 25A (continuous monitoring with a flame ionization detector). A TECO Model 51 was used. The 0 to 100 ppm scale and the 0 to 1000 ppm scale were used for calibrations using zero air, and appropriate low, mid and high range concentrations of EPA protocol propane in nitrogen. Since calibrations are made with propane (C_3H_8), results as methane (CH_4) (or as carbon) are determined by increasing the measured concentration by a factor of three. A continuous trace of VOC as propane was recorded and manually integrated for each 60 minute test period. Instrument calibration was performed initially, and following each 60 minute test period. Any necessary adjustments were made after recording the response of the mid range calibration gas, which was introduced at the inlet to the VOC sampling probe. The gas samples were directed to the heated FID analyzers by way of heated teflon sample lines maintained at a minimum temperature of 250°F.

4.0 DATA REDUCTION

Kirby Forest Industries -- Silsbee OSB Facility
 Press Vent RTO
 PM/VOC Emissions Test - April 27, 1995

Collected Test Data:

RUN 1

RUN 2

RUN 3

Date :	4/27/95	4/27/95	4/27/95
Time start :	1150	1402	1542
Time end :	1251	1502	1642
1. As : sq ft	42.9600	42.9600	42.9600
2. Dn : in.	0.310	0.310	0.310
3. Cp : dimensionless	0.84	0.84	0.84
4. Theta : minutes	60.00	60.00	60.00
5. Y : dimensionless	1.00	1.00	1.00
6. Pbar : in. Hg	29.98	29.98	29.98
7. Pg : in. H2O	0.22	0.22	0.22
8. Vm : cf (dry gas)	69.711	78.864	70.618
9. $\text{sqr}(\text{DP})_{\text{avg}}$: $\text{in. H}_2\text{O}^{.5}$	0.7891	0.9025	0.7966
10. DH : in. H2O	4.3563	5.6188	4.4188
11. ts : degrees F	273.21	276.42	271.96
12. tm : degrees F	108.60	113.90	116.52
13. Vlc : ml	57	70	77
14. CO2 : percent	0.00	0.00	0.00
15. O2 : percent	20.90	20.90	20.90
16. CO : percent	0.00	0.00	0.00
17. VOC : ppm as propane	5.6	5.1	5.2
18. M _{PM} : milligrams			
front half	8.2	8.5	8.6
back half organic	0.9	1.3	0.4
back half aqueous	0.6	0.4	0.6

273.86

5.3

Kirby Forest Industries -- Silsbee OSB Facility
 Press Vent RTO
 PM/VOC Emissions Test - April 27, 1995

Calculations:

		RUN 1	RUN 2	RUN 3	AVG.
1. Pm	: in.Hg (DH/13.6)+Pbar	30.3003	30.3931	30.3049	
2. Ps	: in. Hg (Pg/13.6)+Pbar	29.9962	29.9962	29.9962	
3. An	: sq ft ((Dn/24)*2)(3.1416)	5.24E-04	5.24E-04	5.24E-04	
4. Vmstd	: dscf Vm Y(Pm/Pstd)(Tstd/Tm)	65.556	73.704	65.507	68.256
5. Vwstd	: scf (.04707cf/ml)(Vlc)	2.683	3.295	3.624	
6. Bws	: dimensionless Vwstd/(Vwstd+Vmstd)	0.0393	0.0428	0.0524	0.0448
7. Md	: mol.wt. dry basis .44 CO2+.32 O2+.28(CO+N2)	28.84	28.84	28.84	
8. Ms	: mol.wt. wet basis Md(1-Bws)+18 Bws	28.41	28.37	28.27	
9. Vs	: ft/sec Kp Cp (sqRDP)sqr(Ts/(Ps Ms))	52.56	60.29	53.15	55.33
10. Q	: cfm Vs As(60 sec/min)	135484	155396	136998	142626
11. Qstw	: scfm Q(Ps/Pstd)(Tstd/Ts)	97813	111700	99075	102863
12. Qstd	: dscfm Qstw(1-Bws)	93968	106920	93881	98256
13. I	: percent [(100 Ts)(.002669 Vlc+(Vm Pm/Tm))/(60 theta Vs Ps An)	95.30	94.17	95.32	94.93

Particulate Emissions

14. E,PM	: pounds/hr (M,PM/Vmstd)(Qstd)(60)/(453590)				
front half		1.555	1.631	1.630	1.605
back half organic		0.171	0.249	0.076	0.165
back half aqueous		0.114	0.077	0.114	0.101
Total		1.839	1.957	1.820	1.872
15. C,PM	: grains/dscf (M,PM/Vmstd)(.0154 grains/mg)				
front half		0.0019	0.0018	0.0020	0.0019
back half organic		0.0002	0.0003	0.0001	0.0002
back half aqueous		0.0001	0.0001	0.0001	0.0001
Total		0.0023	0.0021	0.0023	0.0022

VOC Emissions

16. C,VOC	: ppm as C (C,VOC)(3)/(1-Bws)	17.49	15.98	16.46	16.64
17. C,VOC	: #/hr as C (C,VOC)(3.116e-8)(Qstd)(60)	3.07	3.20	2.89	3.05

Kirby Forest Industries - Silsbee, Texas
 Press Vents RTO Inlet
 PM/VOC Inlet Loading Test -- April 27, 1995

Collected Test Data:

	RUN 1	RUN 2	RUN 3
Date :	4/27/95	4/27/95	4/27/95
Time start :	1845	2015	2004
Time end :	1948	2118	2108
1. As : sq ft	26.6667	26.6667	26.6667
2. Dn : in.	0.240	0.240	0.240
3. Cp : dimensionless	0.84	0.84	0.84
4. Theta : minutes	60.00	60.00	60.00
5. Y : dimensionless	1.00	1.00	1.00
6. Pbar : in. Hg	24.75	24.75	24.75
7. Pg : in. H2O	0.65	0.65	0.65
8. Vm : cf (dry gas)	64.291	64.613	67.081
9. $\text{sq}(\text{DP})_{\text{avg}}$: in.H2O ^{0.5}	1.0426	1.0332	1.0739
10. DH : in. H2O	3.8408	3.8104	3.7563
11. ts : degrees F	126.29	129.00	132.88
12. tm : degrees F	107.96	116.04	123.42
13. Vlc : ml	42	45	45
14. CO2 : percent	0.00	0.00	0.00
15. O2 : percent	20.90	20.90	20.90
16. CO : percent	0.00	0.00	0.00
17. VOC : ppm as propane	105.0	88.0	88.0
18. M _{PM} : milligrams			
front half	105.2	47.2	52.7
back half organic	9.6	5.4	6.6
back half aqueous	1.9	1.9	1.8

129.39

93.7

Kirby Forest Industries - Silsbee, Texas
 Press Vents RTO Inlet
 PM/VOC Inlet Loading Test -- April 27, 1995

Calculations:	RUN 1	RUN 2	RUN 3	AVG.
1. Pm : in.Hg (DH/13.6)+Pbar	25.0324	25.0302	25.0262	
2. Ps : in. Hg (Pg/13.6)+Pbar	24.7978	24.7978	24.7978	
3. An : sq ft ((Dn/24)^2)(3.1416)	3.14E-04	3.14E-04	3.14E-04	
4. Vmstd : dscf Vm Y(Pm/Pstd)(Tstd/Tm)	50.004	49.545	50.779	50.110
5. Vwstd : scf (.04707cf/ml)(Vlc)	1.977	2.118	2.118	
6. Bws : dimensionless Vwstd/(Vwstd+Vmstd)	0.0380	0.0410	0.0400	0.0397
7. Md : mol.wt. dry basis .44 CO2+.32 O2+.28(CO+N2)	28.84	28.84	28.84	
8. Ms : mol.wt. wet basis Md(1-Bws)+18 Bws	28.42	28.39	28.40	
9. Vs : ft/sec Kp Cp (sqrDP)sqr(Ts/(Ps Ms))	68.28	67.86	70.76	68.97
10. Q : cfm Vs As(60 sec/min)	109255	108581	113209	110348
11. Qstw : scfm Q(Ps/Pstd)(Tstd/Ts)	81548	80672	83560	81927
12. Qstd : dscfm Qstw(1-Bws)	78447	77365	80214	78675
13. I : percent ((100 Ts)(.002669 Vlc+(Vm Pm/Tm))/(60 theta Vs Ps An)	90.18	90.60	89.56	90.11

Particulate Emissions

14. E,PM : pounds/hr (M,PM/Vmstd)(Qstd)(60)/(453590)				
front half	21.831	9.749	11.012	10.381
back half organic	1.992	1.115	1.379	1.247
back half aqueous	0.394	0.392	0.376	0.384
Total	24.217	11.257	12.767	12.012
15. C,PM : grains/dscf (M,PM/Vmstd)(.0154 grains/mg)				
front half	0.0324	0.0147	0.0160	0.0153
back half organic	0.0030	0.0017	0.0020	0.0018
back half aqueous	0.0006	0.0006	0.0005	0.0006
Total	0.0359	0.0169	0.0185	0.0177

VOC Emissions

16. C,VOC : ppm as C (C,VOC)(3)/(1-Bws)	327.45	275.29	275.01	292.58
17. C,VOC : #/hr as C (C,VOC)(3.116e-8)(Qstd)(60)	48.03	39.82	41.24	43.03

5.0 NOMENCLATURE

SYMBOL	UNITS	DESCRIPTION
A_n	ft ²	Nozzle cross sectional area
A_s	ft ²	Stack cross sectional area
B_{ws}	dimensionless	Wet gas fraction
CO_2	percent	Carbon dioxide content by volume
CO	percent	Carbon monoxide content by volume
C_p	dimensionless	Pitot correction factor
C_X	as labeled	Concentration of pollutant X
DGF	dimensionless	Dry gas fraction
D_n	inches	Nozzle diameter
ΔH (delta H)	in. H ₂ O	Pressure drop across meter orifice
ΔP (delta P)	in. H ₂ O	Stack gas velocity pressure
E_X	#/hr	Emission rate of pollutant X
EX	#/MM Btu	Emission rate of pollutant X
F	dscf	Volume of flue gas per MM Btu
I	percent	Nozzle velocity/stack gas velocity
K_p	consistent	Pitot tube constant
M_X	milligrams	Sample weight of pollutant X
M_d	## mole	Dry molecular weight of stack gas
M_s	## mole	Wet molecular weight of stack gas
N_2	percent	Nitrogen content by volume, dry basis
O_2	percent	Oxygen content by volume, dry basis
P_{bar}	in. Hg	Barometric pressure
P_g	in. Hg	Stack static pressure
P_m	in. Hg	Total pressure at meter ($P_{bar} + (\Delta H/13.6)$)
P_s	in. Hg	Total stack pressure ($P_{bar} + (P_g/13.6)$)
P_{std}	in. Hg	Standard barometric pressure = 29.92
Q	acfm	Volumetric flow rate at stack conditions
Q_{std}	dscfm	Volumetric flow rate at standard conditions, dry basis
Q_{stdw}	scfm	Volumetric flow rate at standard conditions, wet basis
θ (theta)	minutes	Sample duration
t_m	°F	Meter temperature (T_m denotes °R)
t_s	°F	Stack temperature (T_s denotes °R)
T_{std}	°R	Standard temperature = 528°R
V_{lc}	ml	volume of water collected
V_m	ft ³	Volume of dry gas sampled through meter
V_{mstd}	dscf	Sample volume at standard conditions
V_{wstd}	scf	Sample volume of water vapor
Y	dimensionless	Meter coefficient
X_{sair}	percent	Excess air

6.0 CALIBRATIONS:

Measurement devices used by Environmental Monitoring Laboratories and subject to changes in measurement precision are initially calibrated prior to use. Those instruments for which calibration factors are subject to change or for which calibration checks are required, are calibrated following each field use or as otherwise directed and noted. Calibration procedures for specific equipment are as follows.

Dry Gas Meter:

Dry gas meters are periodically removed from the sampling consoles and cleaned and repaired (new gaskets etc. as required). Following the overhaul of a meter, the measuring precision is checked by the Bell Prover Method and adjusted when necessary to read to within 2% of 100% accuracy. This service is provided by Big Three Meter Company in Jackson, Mississippi. Overhaul service or any six month period is followed by a five point calibration described in APTD-0576 using either a wet test meter or calibrated dry gas meter (used exclusively for calibrations) as a standard reference. Following field use, a gas meter calibration is checked in one of two ways. [1] Three calibration checks at intermediate orifice settings are performed or [2] orifice meter coefficients are used.

If a meter coefficient obtained from pre-test and post-test checks differs by more than 5%, the coefficient (Y) giving the lower sample volume is used in the calculations.

Orifice:

The orifice coefficient is initially determined and is rechecked following a major gas meter repair and calibration.

Nozzles:

Nozzles are checked before each field use with a precision (.001 in.) dial caliper. Three measurements on different axes are made; an average of those three readings is used in calculations. If the tolerance among measurements exceeds 0.004 inches (highest to lowest reading) the nozzle is repaired and recalibrated or discarded.

Pitot Tubes:

Pitot tubes meeting EPA geometry standards are assigned a coefficient of 0.84. Pitot tubes are visually inspected for damage before, during and after use. Those pitot tubes not meeting the geometry standards are assigned a coefficient from the manufacturer's calibration which it retains unless damaged. All pitot tubes used by Environmental Monitoring Laboratories are manufactured by NAPP, Inc.

Temperature Measuring Instruments:

Most temperature measurements are made with a type K thermocouple and an Omega digital thermocouple thermometer which has an initial calibration traceable to NBS. Other measurements are made using bimetallic dial thermometers. The thermocouples and dial thermometers are checked following or during a test series against an ASTM mercury in glass thermometer.

Barometer:

Aneroid field barometers are checked against and adjusted to readings from a mercury barometer or readings obtained from local weather authorities.

Differential Pressure Gauges:

Velocity head (ΔP) and orifice pressure differential (ΔH) measurements are made using water manometers of the appropriate range unless otherwise noted in the test data. Manometers do not require calibration.

7.0 APPENDICES

A. Field and Laboratory Data

B. Calibrations

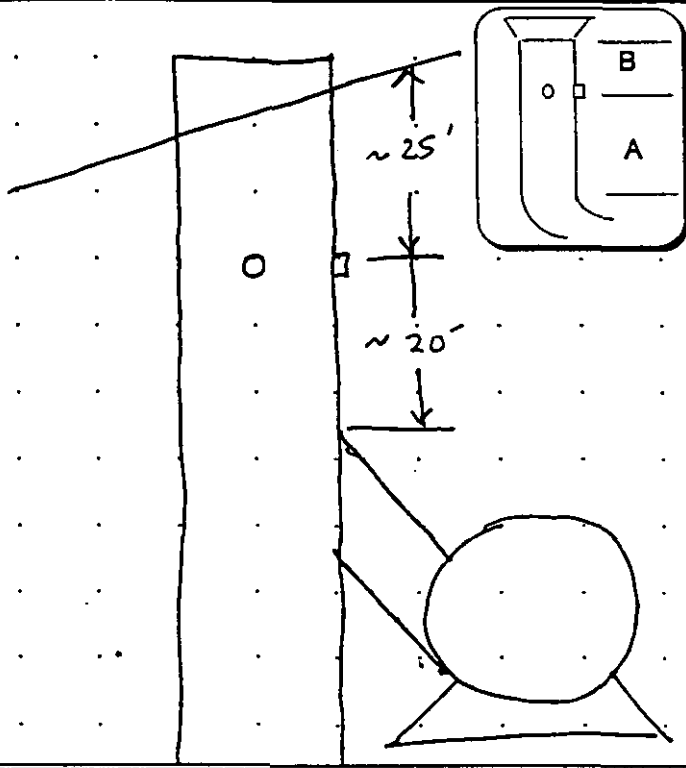
C. VOC Recorder Traces

STACK CONFIGURATION AND SAMPLE POINT LAYOUT FOR CIRCULAR STACKS

PLANT: Kirby Forest Industries - Silas OSB
SOURCE: Press Vanta RTQ outlet
TEST FOR: PM/VOC
TEST OPERATORS: Russell/G. McKnight/B. McKnight

Date: 4-27-95

SKETCH OF STACK



PERCENT OF DIAMETER

	points on a diameter							
	2	4	6	8	10	12	14	16
point no.								
1	_____ 14.6	6.7	4.4	3.2	2.6	2.1	1.8	1.6
2	_____ 85.4	25.0	14.6	10.5	8.2	6.7	5.7	4.9
3	_____ 75.0	29.6	19.4	14.6	11.8	9.9	8.5	
4	_____ 93.3	70.4	32.3	22.6	17.7	14.6	12.5	
5	_____ 85.4	67.7	34.2	25.0	20.1	16.9		
6	_____ 95.6	80.6	65.8	35.6	26.9	22.0		
7	_____ 89.5	77.4	64.4	36.6	28.3			
8	_____ 96.8	85.4	75.0	63.4	37.5			
9	_____ 91.8	82.3	73.1	62.5				
10	_____ 97.4	88.2	79.9	71.7				
11	_____ 93.3	85.4	78.0					
12	_____ 97.9	90.1	83.1					
13	_____ 94.3	87.5						
14	_____ 98.2	91.5						
15	_____ 95.1							
16	_____ 98.4							

STACK DIAMETER:

89.75"

Distance from ports to disturbance:

A. to upstream disturbance

B. to downstream disturbance

Upstream diameters:

Downstream diameters:

Minimum No. sample points required:

No. sample points selected:

Port Length:

5.25"

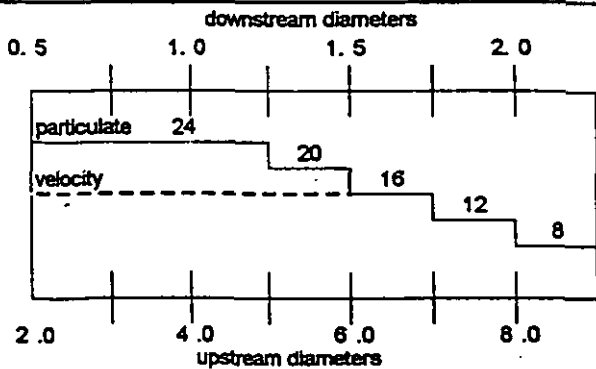
Port Type:

4" pipe nipple

Port Access:

plot/area - 11

MINIMUM NO. OF POINTS ON A DIAMETER



Point No.	inches from wall	velocity head
--------------	---------------------	---------------

1	1.9	
2	6.0	
3	10.6	
4	15.9	
5	22.4	
6	32.0	
7	57.8	
8	67.3	
9	73.9	
10	79.2	
11	83.7	
12	87.9	

Pitot ID : _____ Pitot Cp: _____ Stack Temp: 7.85

Remarks:

$\Delta p \sim .4 \rightarrow .6$

Plant Louisiana Pacific - Ruby Forest Dist. - Silsbee OSB
 Sampling Location Pump House Outlet RTO
 Test For PM/VOC
 Test Operators Russell B. McKnight

RUN No. 1
 Date 4-27-95
 Time start 1150 end 1251

A. Box Anderson
 Sample Box No. 4
 Probe/Pitot 8'55
 Pitot Cp .24
 Nozzle Dia. 3/0
 Filter No.
 Amb. Temp. °F 80 ~ 80
 Bar. Press. "Hg 29.99
 Static Press. "H₂O .22

No. Sample Pts. 12 x 2
 Minutes/Pt. 2.5
 NOMOGRAPH
 ΔH@ 1.75
 Meter Temp. 100
 % H₂O 13
 C-Factor .89
 Stack Temp. 285
 Ref. ΔP 1.28

Gas Analysis Est.
 CO₂
 O₂
 CO
 Time
 Condensate: 251
 tare 200 fin 251
 Silica gel:
 tare 734 fin 740

Remarks:

Port Point	El. Time, Min.	DGM Reading, Ft.	Velocity Head ΔP, in. H ₂ O	Orifice ΔH, in. H ₂ O	Stack Temp. °F	Meter Temp. °F In Out	Oven Temp. °F	Imp. Temp. °C	Vac. in. Hg
1	000	477.22	0.38	2.50	278	84 89	261	69	2
2	230	479.5	0.37	2.50	269	92 89	256	66	2
3	500	481.1	0.33	2.20	283	97 89	250	60	2
4	730	483.6	0.27	2.45	267	102 85	255	60	2
5	1000	485.9	0.48	3.20	282	107 86	260	60	2
6	1230	488.1	0.50	3.30	270	111 87	260	63	2
7	1500	490.8	0.88	5.50	266	116 90	260	62	2
8	1730	493.6	0.95	6.50	277	119 92	249	63	2
	2000	496.9	1.00	6.90	281	121 93	252	65	4
10	2230	500.7	1.00	6.90	270	123 96	253	65	4
11	2500	504.5	0.92	6.10	266	125 99	249	65	4
12	2730	507.9	0.76	5.00	269	124 100	256	66	4
1	3000	511.4	0.75	5.00	275	124 102	251	65	4
2	230	514.7	0.84	5.50	262	125 103	250	65	4
3	500	517.9	1.00	6.70	283	127 105	253	65	4
4	730	521.2	1.00	6.70	278	128 106	247	65	2
5	1000	525.1	0.96	6.60	286	128 108	252	65	2
6	1230	528.6	0.90	6.00	264	129 109	250	65	2
7	1500	533.1	0.48	3.20	266	129 110	251	65	2
8	1730	535.5	0.37	2.45	271	126 111	252	65	2
9	2000	538.0	0.35	2.25	267	126 111	250	65	2
10	2230	540.8	0.33	2.20	275	124 111	257	66	2
11	2500	542.2	0.38	2.50	277	123 111	251	66	2
12	2730	544.4	0.35	2.40	275	124 112	251	65	2
and	60	546.933							

Sub. Check: OSI → .062 = .014 @ 8" Hg

69711

7891

4.3563

273.21

108.60

Plant Kalby Forest Industries - Silas OSBSampling Location Pine Knots RTOTest For PM/VOCTest Operators Russell/B. McKnightRUN No. 2Date 4-27-95Time start 1402 end 1502A Box Anderson
Sample Box No. 3
Probe/Pitot 8" SS
Pitot Cp .84
Nozzle Dia. .310
Filter No. _____No. Sample Pts. 12x2
Minutes/Pt. 2.5

NOMOGRAPH

 $\Delta H @$ 1.75

Meter Temp. _____

% H₂O _____

C-Factor _____

Stack Temp. _____

Ref. ΔP .28

Gas Analysis

CO₂ _____O₂ _____

CO _____

Time _____

Condensate:

tare 200 fin 245

Silica gel:

tare 680 fin 705

Remarks: _____

Amb. Temp. °F 64.85

Bar. Press. "Hg _____

Static Press. "H₂O -.22

Port Point	El. Time, Min.	DGM Reading, Ft.	Velocity Head ΔP , in. H ₂ O	Orifice ΔH , in. H ₂ O	Stack Temp. °F	Meter Temp., °F In Out	Oven Temp. °F	Imp. Temp. °F	Vac in. Hg
1	000	547.451	0.37	2.45	274	91 91	253	67	2
2	230	549.3	0.34	2.20	281	93 91	250	66	2
3	500	551.6	0.38	2.50	281	98 90	251	65	2
4	730	553.6	0.35	2.30	281	102 91	253	65	2
5	1000	556.0	0.44	2.90	277	106 92	251	64	2
6	1230	558.3	0.43	2.80	271	109 94	250	64	2
7	1500	560.9	0.90	6.00	284	110 95	253	65	2
8	1730	564.1	0.95	6.40	269	122 98	250	65	2
	2000	567.6	1.05	7.00	286	126 100	248	65	2
10	2230	571.1	1.10	7.40	285	129 102	252	65	4
11	2500	576.0	0.96	6.40	275	130 106	250	65	4
12	2730	578.7	0.87	5.75	275	130 106	253	65	3
1	000	582.7	0.93	5.85	275	130 108	254	65	3
2	230	585.9	1.05	7.00	276	131 110	253	66	4
3	500	590.6	1.05	7.00	285	133 111	253	66	4
4	730	593.7	1.05	7.00	271	132 113	255	66	4
5	1000	596.8	1.10	7.40	265	134 113	249	65	4
6	1230	601.0	0.95	6.30	269	134 114	248	65	4
7	1500	604.7	0.88	5.80	292	134 114	250	65	4
8	1730	608.1	0.97	6.40	271	133 115	249	65	4
9	2000	610.8	1.15	7.70	276	133 115	247	65	4
10	2230	614.5	1.05	7.40	271	134 117	251	66	4
11	2500	619.0	0.94	6.30	271	135 118	252	66	4
12	2730	622.8	0.96	6.60	273	135 118	251	65	4
and	66	626.315							

Back check: $.035 \rightarrow .037 = .002$ per ft

78.864

.9025

5.6188

276.42

113.90

Plant _____	RUN No. <u>3</u>
Sampling Location <u>PRESS VENTS RTO</u>	Date _____
Test For _____	Time start <u>1542</u> end <u>1642</u>
Test Operators _____	

M. Box _____	No. Sample Pts. _____	Gas Analysis _____	Remarks: _____ _____ _____ _____ _____ _____
Sample Box _____	Minutes/Pt. _____	CO ₂ _____	
Probe/Pitot _____		O ₂ _____	
Pitot Cp _____	NOMOGRAPH _____	CO _____	
Nozzle Dia. _____	Δ H @ _____	Time _____	
Filter No. _____	Meter Temp. _____	Condensate: _____	
Amb. Temp. °F _____	% H ₂ O _____	tare <u>200</u> fin <u>241</u>	
Bar. Press. "Hg _____	C-Factor _____	Silica gel: _____	
Static Press. "H ₂ O _____	Stack Temp. _____	tare <u>678</u> fin <u>714</u>	
	Ref. Δ P _____		

Port Point	El. Time, Min.	DGM Reading, Ft.	Velocity Head Δ P, in. H ₂ O	Orifice Δ H in. H ₂ O	Stack Temp. °F	Meter Temp., °F		Oven Temp. °F	Imp. Temp. °F	Vac in. Hg
						In	Out			
1	000	626.725	0.40	2.60	271	97	99	249	65	2
2	230	629.0	0.40	2.60	274	99	99	248	64	2
3	560	631.3	0.37	2.45	269	103	98	252	64	2
4	730	633.6	0.34	2.20	277	106	98	249	64	2
5	1000	635.8	0.36	2.40	270	110	98	254	64	2
6	1230	638.1	0.46	3.00	289	113	99	254	64	2
7	1500	640.6	0.81	5.50	285	120	100	249	64	3
8	1730	643.8	0.95	6.40	282	125	103	251	64	4
9	2000	647.6	1.00	6.70	275	129	105	245	63	4
10	2230	651.1	1.00	6.70	272	131	107	259	63	4
11	2500	654.8	0.90	6.00	270	123	109	255	63	4
12	2730	659.3	1.10	7.50	270	134	110	254	63	4
1	3000	662.050	0.50	3.30	280	134	112	255	63	4
2	230	664.8	0.40	2.60	283	130	113	250	63	4
3	500	667.3	0.40	2.70	283	128	115	250	63	4
4	730	669.7	0.35	2.30	250	128	113	250	63	4
5	1000	671.8	0.36	2.40	284	126	114	250	63	2
6	1230	674.4	0.45	3.00	280	127	115	250	63	2
7	1500	676.8	0.50	3.30	270	129	116	251	63	2
8	1730	679.6	1.00	6.00	272	132	116	251	63	2
9	2000	682.5	0.97	6.50	271	135	117	270	62	2
10	2230	686.5	0.99	6.70	252	138	118	248	62	2
11	2500	689.8	1.00	6.70	250	138	119	255	62	2
12	2730	693.5	0.78	4.50	248	138	119	249	62	2
nd	60	697.343								

LEAK CHECK: 090 → 093 = .003 in. 27 1/2

70.48 .7966 4.4188 21.94 116.52

PARTICULATE CATCH ANALYSIS

SAMPLES:

Kirby - 5 Subur OSB Pm Vent RTO

DATE TAKEN:

4-27-95 DATE ANALYZED:

4-29-95

DELIVERED BY:

202

RECEIVED BY:

202

ANALYZED BY:

202

(Attach chain of custody if additional exchanges occur)

FILTERS:

RUN NO.	1	2	3	
FILTER NO.	2670	2756	2672	
FILTER TARE, gms.	.5645	.5665	.5542	
	.5681	.5699	.5570	
	.5680	.5700	.5570	
FINAL WEIGHT, gms.	.5680	.5700	.5570	
NET GAIN, gms.	.0035	.0035	.0028	

PROBE WASH:

RUN NO.	1	2	3	
CONTAINER I.D.	RTO R1	RTO R2	RTO R3	
VOLUME INTACT?	—	✓	—	
VOLUME, ml	180	200	150	
	(J)	(65)	(J)	()
TARE WEIGHT, gms.	104.4062	114.7836	104.6244	
	104.4111	114.7886	104.6301	
	104.4109	114.7886	104.6302	
FINAL WEIGHT, gms.	104.4109	114.7886	104.6302	
NET GAIN, gms.	.0047	.0050	.0058	
LESS BLANK, gms.				

PARTICULATE SAMPLE WEIGHT:

RUN NO.	1	2	3	
filter + probe, mg.	8.2	8.5	8.6	

0.0082 g

0.0085 g

0.0086 g

Methylene Chloride Extraction

ANALYZED BY:

KFI - Silsbee OSB - Press/Vent/RTD

4-~~27~~²⁷-95 DATE ANALYZED: 5-5-95

RECEIVED BY: 

DAR

(Attach chain of custody if additional exchanges occur)

RUN NO.	1	2	3	
CONTAINER I.D.	RTO R1	RTO R2	RTO R3	
VOLUME INTACT?	✓	✓	✓	
VOLUME, ml	270	270	270	

	(1)	(86)	(2)	()
TARE WEIGHT, gms.	103.1821	108.1468	107.7533	
	103.1833	108.1481	107.7539	
	103.1830	108.1481	107.7537	
FINAL WEIGHT, gms.	103.1830	108.1481	107.7537	
less blank, gms.				
NET GAIN, milligrams	.0009 (g)	.0013 (g)	.0004 (g)	

	(83)	(56)	(68)	()
TARE WEIGHT, gms.	105.1047	105.8161	112.5344	
	105.1057	105.8164	112.5353	
	105.1053	105.8165	112.5350	
FINAL WEIGHT, gms.	105.1053	105.8165	112.5350	
less blank, gms.				
NET GAIN, milligrams	0.0056 g 0.6	0.4	0.6	

0.0006 g

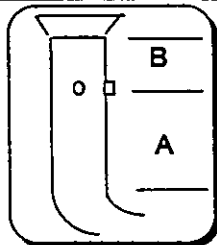
0.0004 g

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STACK CONFIGURATION AND SAMPLE POINT LAYOUT FOR CIRCULAR STACKS

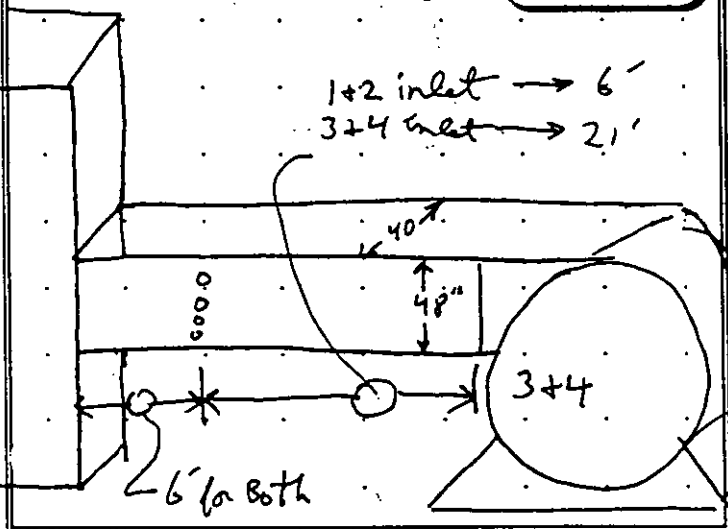
PLANT: Kirby Forest Industries - Silasbee DSB Date: 4-27-95
SOURCE: Press Vents RTO Inlet
TEST FOR: PM/VOC
TEST OPERATORS: Russell/B. McKnight / G. McKnight

SKETCH OF STACK



2 identical inlets.
to knock out chamber

1+2 inlet $\rightarrow 6'$
3+4 inlet $\rightarrow 21'$



PERCENT OF DIAMETER

points on a diameter

point no.	2	4	6	8	10	12	14	16
1	14.6	6.7	4.4	3.2	2.6	2.1	1.8	1.6
2	85.4	25.0	14.6	10.5	8.2	6.7	5.7	4.9
3	75.0	29.6	19.4	14.6	11.8	9.9	8.5	
4	93.3	70.4	32.3	22.6	17.7	14.6	12.5	
5	85.4	67.7	34.2	25.0	20.1	16.9		
6	95.6	80.6	65.8	35.6	26.9	22.0		
7	89.5	77.4	64.4	36.6	28.3			
8	96.8	85.4	75.0	63.4	37.5			
9	91.8	82.3	73.1	62.5				
10	97.4	88.2	79.9	71.7				
11	93.3	85.4	78.0					
12	97.9	90.1	83.1					
13		94.3	87.5					
14		98.2	91.5					
15			95.1					
16			98.4					

STACK DIAMETER:

40 x 48

Distance from ports to disturbance:

A. to upstream disturbance

B. to downstream disturbance

Upstream diameters:

Downstream diameters:

Minimum No. sample points required:

No. sample points selected:

Port Length:

4.5"

Port Type:

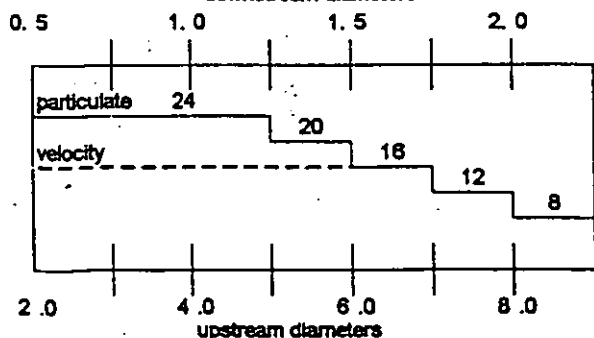
3" pine nipple

Port Access:

Fork Lift Board

MINIMUM NO. OF POINTS ON A DIAMETER	
1	1
2	2
3	3
4	4
5	5
6	6
7	7
8	8
9	9
10	10
11	11
12	12
13	13
14	14
15	15
16	16
17	17
18	18
19	19
20	20
21	21
22	22
23	23
24	24
25	25
26	26
27	27
28	28
29	29
30	30
31	31
32	32
33	33
34	34
35	35
36	36
37	37
38	38
39	39
40	40
41	41
42	42
43	43
44	44
45	45
46	46
47	47
48	48
49	49
50	50
51	51
52	52
53	53
54	54
55	55
56	56
57	57
58	58
59	59
60	60
61	61
62	62
63	63
64	64
65	65
66	66
67	67
68	68
69	69
70	70
71	71
72	72
73	73
74	74
75	75
76	76
77	77
78	78
79	79
80	80
81	81
82	82
83	83
84	84
85	85
86	86
87	87
88	88
89	89
90	90
91	91
92	92
93	93
94	94
95	95
96	96
97	97
98	98
99	99
100	100

downstream diameters



Point No.	Inches from wall	velocity head
-----------	------------------	---------------

[illegible]

Pilot ID : Pilot Cp: Stack Temp:

Remarks:

Plant Fifty Forest Industries - Silokea OSB
 Sampling Location Line 1 to RTO inlet
 Test For PAH/VOC
 Test Operators Russell

RUN No. 1
 Date 4-27-95
 Time start 1149 end 1301

Box PAC
 Sample Box No. 2
 Probe/Pitot 4.55
 Pitot Cp .84
 Nozzle Dia. 240
 Filter No. 2
 Amb. Temp. °F 80
 Bar. Press. "Hg
 Static Press. "H₂O

No. Sample Pts. (9x4)x2
 Minutes/Pt. 2.5
 NOMOGRAPH
 ΔH@ 1.90
 Meter Temp. 100
 % H₂O >10
 C-Factor 1.0
 Stack Temp. 125
 Ref. ΔP .57

Gas Analysis AIR
 CO₂
 O₂
 CO
 Time
 Condensate:
 tare 200 fin 228
 Silica gel:
 tare 699 fin 713

Remarks:

Port Point	El. Time, Min.	DGM Reading, Ft. ³	Velocity Head ΔP, in. H ₂ O	Orifice ΔH in. H ₂ O	Stack Temp. °F	Meter Temp., °F In Out	Oven Temp. °F	Imp. Temp. °F	Vac. in. Hg
1	060	397.000	1.40	4.50	128	88 86	248	60	2
2	230	399.6	1.80	6.00	127	89 86	254	56	2
3	500	403.7	1.80	6.00	125	87 91	259	59	2
1	730	406.5	0.66	1.90	125	98 90	250	59	2
2	730	408.3	0.60	2.20	128	101 90	253	60	2
3	500	411.4	1.00	3.25	123	107 89	255	60	2
1	1500	412.7	0.82	2.65	126	106 92	251	62	2
2	230	416.0	1.40	4.70	127	113 93	248	65	2
3	500	419.1	1.20	3.50	125	112 92	251	64	2
1	230	421.747	0.15	0.48	126	116 97	252	64	2
2	230	423.3	0.95	3.00	128	119 96	250	64	2
3	500	425.9	1.00	3.25	124	120 97	251	65	2
1	300	428.0	0.82	2.65	126	121 99	250	65	2
2	230	430.8	1.40	4.50	127	121 100	251	65	2
3	500	433.1	1.30	4.20	125	128 102	265	65	2
1	370	435.8	1.10	3.60	126	122 100	260	65	2
2	230	438.5	1.70	5.50	125	130 103	261	65	2
3	500	441.8	1.30	4.20	128	132 105	260	65	2
1	450	444.6	1.20	3.90	130	131 105	261	65	2
2	230	447.4	1.50	4.80	125	136 108	250	65	2
3	500	449.9	1.50	4.80	130	138 109	230	65	2
1	520	453.682	0.70	2.30	125	135 108	225	65	2
2	230	455.9	0.20	3.90	126	117 109	220	65	2
3	500	458.7	1.05	3.40	126	140 111	200	65	2
60		461.291							
CHECK: 058 → 066 = 002 @ 5.48									
64291		110426		3,8408	126.29		10796		

Plant Kidby Forest Industries - Silaboa C&D
 Sampling Location Pure Vents RTO 2nd
 Test For PM/VOC
 Test Operators Russell/C. McKnight

RUN No. 2
 Date 4-27-95
 Time start 1401 end 1504

Box RAC
 Sample Box No. 1
 Probe/Pitot 4' SS
 Pitot Cp .84
 Nozzle Dia. .240
 Filter No.
 Amb. Temp. °F 80.5 = 85
 Bar. Press. "Hg
 Static Press. "H₂O .65

No. Sample Pts. (3x4)x(2)
 Minutes/Pt. 2.5

NOMOGRAPH
 ΔH@ 1.95
 Meter Temp.
 % H₂O
 C-Factor
 Stack Temp.
 Ref. ΔP .57

Gas Analysis AIR
 CO₂
 O₂
 CO
 Time

Condensate:
 tare 200 fin 230
 Silica gel:
 tare 715 fin 730

Remarks:

Port Point	El. Time, Min.	DGM Reading, Ft. ²	Velocity Head ΔP, in. H ₂ O	Orifice ΔH in. H ₂ O	Stack Temp. °F	Meter Temp. °F in	Meter Temp. °F Out	Oven Temp. °F	Imp. Temp. °F	Vac. in. Hg
1	000	461.672	1.10	3.55	122	102	101	248	68	2
2	230	464.5	1.40	4.50	122	109	102	252	64	2
3	500	467.1	1.20	3.90	124	107	102	249	60	2
1	730/0	469.7	0.88	2.85	121	109	102	254	62	2
2	230	472.2	1.65	5.20	125	108	105	247	62	2
3	500	475.1	1.40	4.50	122	107	102	253	63	2
1	0	478.0	1.00	3.20	124	118	103	249	63	2
2	230	480.8	1.60	5.20	125	120	103	250	63	2
3	500	483.8	1.40	4.50	125	127	104	250	65	2
1	0	486.9	0.86	2.80	129	126	107	259	63	2
2	230	490.3	1.50	7.45	128	131	105	250	64	2
3	500	491.9	1.15	3.70	127	132	107	253	64	2
1	0	494.3	1.55	5.00	130	129	107	251	63	2
2	230	497.8	1.75	5.70	131	129	108	253	65	2
3	500	500.9	1.40	4.50	136	130	109	250	63	2
1	0	502.8	0.70	2.30	134	133	109	251	63	2
2	230	506.1	1.60	5.00	135	134	111	252	63	2
3	500	509.1	0.95	3.10	131	136	112	251	64	2
1	0	512.0	0.86	2.80	130	136	111	250	65	2
2	230	514.4	0.35	4.30	134	136	109	253	65	2
3	500	516.8	0.94	3.10	136	138	108	254	65	2
1	0	519.4	0.59	1.90	134	135	113	259	66	2
2	230	521.5	0.96	3.10	136	136	113	251	65	2
3	500	522.9	0.98	3.20	135	136	113	250	65	2
60		526.285								
Red check: 0.66 → 0.86 = 0.20 <u>4' 3" H</u> 64.613 1.0332 3.8104 129.00 116.04										

Plant _____
 Sampling Location PRESS VENTS EO - INLET

Test For _____

Test Operators _____

RUN No. 3

Date _____

Time start 1542 end _____

h Box _____	No. Sample Pts. _____	Gas Analysis _____	Remarks: _____ _____ _____ _____ _____ _____
Sample Box _____	Minutes/Pt. _____	CO ₂ _____	
Probe/Pitot _____	NOMOGRAPH _____	O ₂ _____	
Pitot Cp _____	Δ H @ _____	CO _____	
Nozzle Dia. _____	Meter Temp. _____	Time _____	
Filter No. _____	% H ₂ O _____	Condensate: _____	
Amb. Temp. °F _____	C-Factor _____	tare <u>200</u> fin <u>232</u>	
Bar. Press. "Hg _____	Stack Temp. _____	Silica gel: _____	
Static Press. "H ₂ O _____	Ref. Δ P _____	tare <u>733</u> fin <u>746</u>	

Port Point	El. Time, Min.	DGM Reading, Ft. ³	Velocity Head Δ P, in. H ₂ O	Orifice Δ H in. H ₂ O	Stack Temp. °F	Meter Temp., °F In Out	Oven Temp. °F	Imp. Temp. °F	Vac. in. Hg
1	000	528.589	1.50	4.80	134	120 113	249	60	2
2	230	533.7	1.70	5.50	135	143 108	249	60	2
3	500	536.9	1.40	4.50	135	123 110	255	60	2
1	0	539.925	0.80	2.60	135	127 108	250	60	2
2	230	542.1	1.50	4.80	133	132 109	254	61	2
3	500	545.2	1.20	3.90	132	130 109	252	61	2
1	0	548.048	0.80	2.60	133	131 110	246	61	2
2	230	550.4	1.30	4.20	134	132 109	252	61	2
3	500	553.4	1.10	3.50	131	134 111	259	61	2
1	0	556.100	0.51	1.65	136	134 110	254	61	2
2	230	557.9	0.85	2.80	133	133 112	255	61	2
3	500	560.2	0.98	2.55	135	130 111	253	61	2
1	0	562.410	1.10	3.60	135	135 113	253	61	2
2	230	565.4	1.50	4.80	132	135 111	250	61	2
3	500	568.2	1.20	3.85	131	140 114	251	60	2
1	0	570.999	1.20	3.85	130	135 112	251	60	2
2	230	574.0	1.20	3.85	132	136 113	251	60	2
3	500	576.5	1.10	3.60	131	151 115	250	65	2
1	0	579.115	0.90	2.90	129	136 111	250	65	2
2	230	581.6	1.50	4.80	131	136 114	248	66	2
3	500	586.4	1.20	3.90	131	136 114	248	66	2
1	0	587.499	0.80	2.60	133	140 114	248	66	2
2	230	589.8	1.40	4.50	133	143 119	248	65	2
3	500	592.7	1.40	4.50	135	143 119	248	65	2
4	60	595.670							

67.081 $\frac{0.008 \times 0.028}{0.035} = 0.008 \text{ in. } 0.5 \frac{1}{8}$
 1.0739 3.7563 13288 12342

PARTICULATE CATCH ANALYSIS

SAMPLES:

Kirby - Silsbee OSB Presumably RTO & R2

DATE TAKEN:

4-27-95 DATE ANALYZED: 7-25-95

DELIVERED BY:

PCR

RECEIVED BY:

PCR

ANALYZED BY:

PCR

(Attach chain of custody if additional exchanges occur)

FILTERS:

No. 1 had oily spot - may have been contaminated

RUN NO.	1	2	3	
FILTER NO.	2671	2755	2673	
FILTER TARE, gms.	.5633	.5611	.5647	
	.6504	.5896	.5991	
	.6502	.5896	.5919	
FINAL WEIGHT, gms.	.6502	.5896	.5989	
NET GAIN, gms.	.0869	.0285	.0342	

PROBE WASH:

RUN NO.	1	2	3	
CONTAINER I.D.	RTO R1(N)	RTO(N) R2	RTO R3(N)	
VOLUME INTACT?	✓	✓	✓	
VOLUME, ml	160	150	210	
	(7)	(45)	(84)	()
TARE WEIGHT, gms.	111.5422	107.2485	105.3508	
	111.5609	107.2670	105.8694	
	111.5605	107.2672	105.8693	
	111.5605	107.2672	105.8693	
FINAL WEIGHT, gms				
NET GAIN, gms.	.0183	.0187	.0185	
LESS BLANK, gms.				

PARTICULATE SAMPLE WEIGHT:

RUN NO.	1	2	3	
filter + probe, mg.	105.2	47.2	52.7	

0.0472 g

0.0527 g

BACK HALF PARTICULATE CATCH ANALYSIS

Methylene Chloride Extraction

SAMPLES:

KFI - Silica OSB Pass Vent RTO Inlet

DATE TAKEN:

4-22-95

DATE ANALYZED:

5-5-95

DELIVERED BY:

DDR

RECEIVED BY:

DDR

ANALYZED BY:

DDR

(Attach chain of custody if additional exchanges occur)

RUN NO.	1	2	3	
CONTAINER ID.	SL20SB R1 I	R2 I	R3 I	
VOLUME INTACT?	✓	✓	✓	
VOLUME, ml	~ 280	280	280	

Organic Fraction

TARE WEIGHT, gms.	(89) 106.4077	(4) 108.4567	(90) 27 98.8416	()
	106.4175	108.4622	98.8474	
	106.4113	108.4621	98.8482	
FINAL WEIGHT, gms.	106.4173	108.4621	98.8482	
less blank, gms.				
NET GAIN, milligrams	9.6	5.4	6.6	

0.0096 g

0.0054 g

0.0066 g

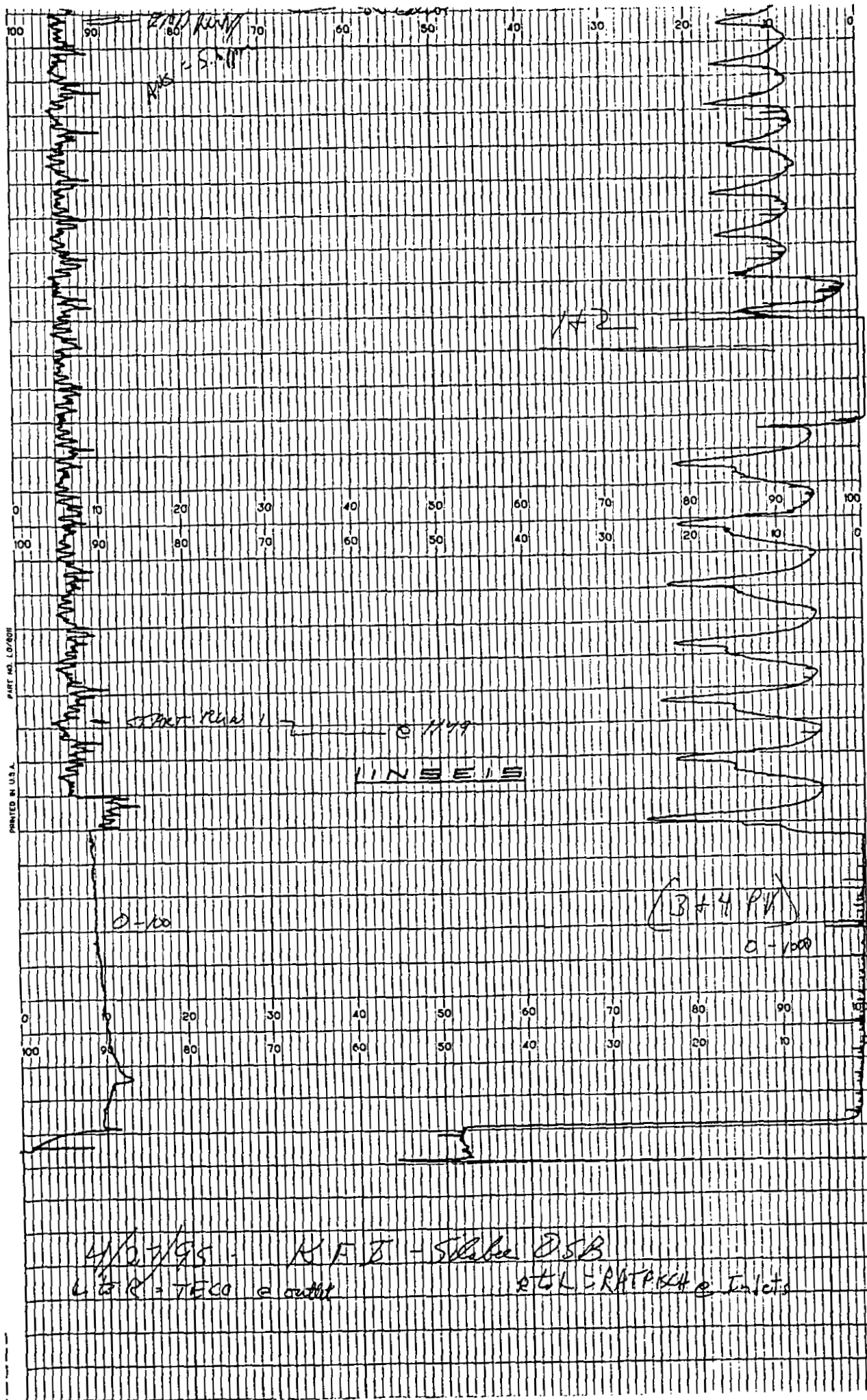
Aqueous Fraction

TARE WEIGHT, gms.	(9) 114.8150	(89) 109.1524	(91) 102.7993	()
FINAL WEIGHT, gms.	114.8169	109.1543	102.8011	
less blank, gms.				
NET GAIN, milligrams	1.9	1.9	1.8	

0.0019 g

0.0019 g

0.0018 g



PRINTED IN U.S.A.
PART NO. LD/80H

4/27/95 - K.F.D. - Scribe DSB
L & R = TECO @ output R & L = R.A.P.S.4 @ Inputs

INSEIS

CR
to 344 PVA

0-100
PVA

START 62-1100

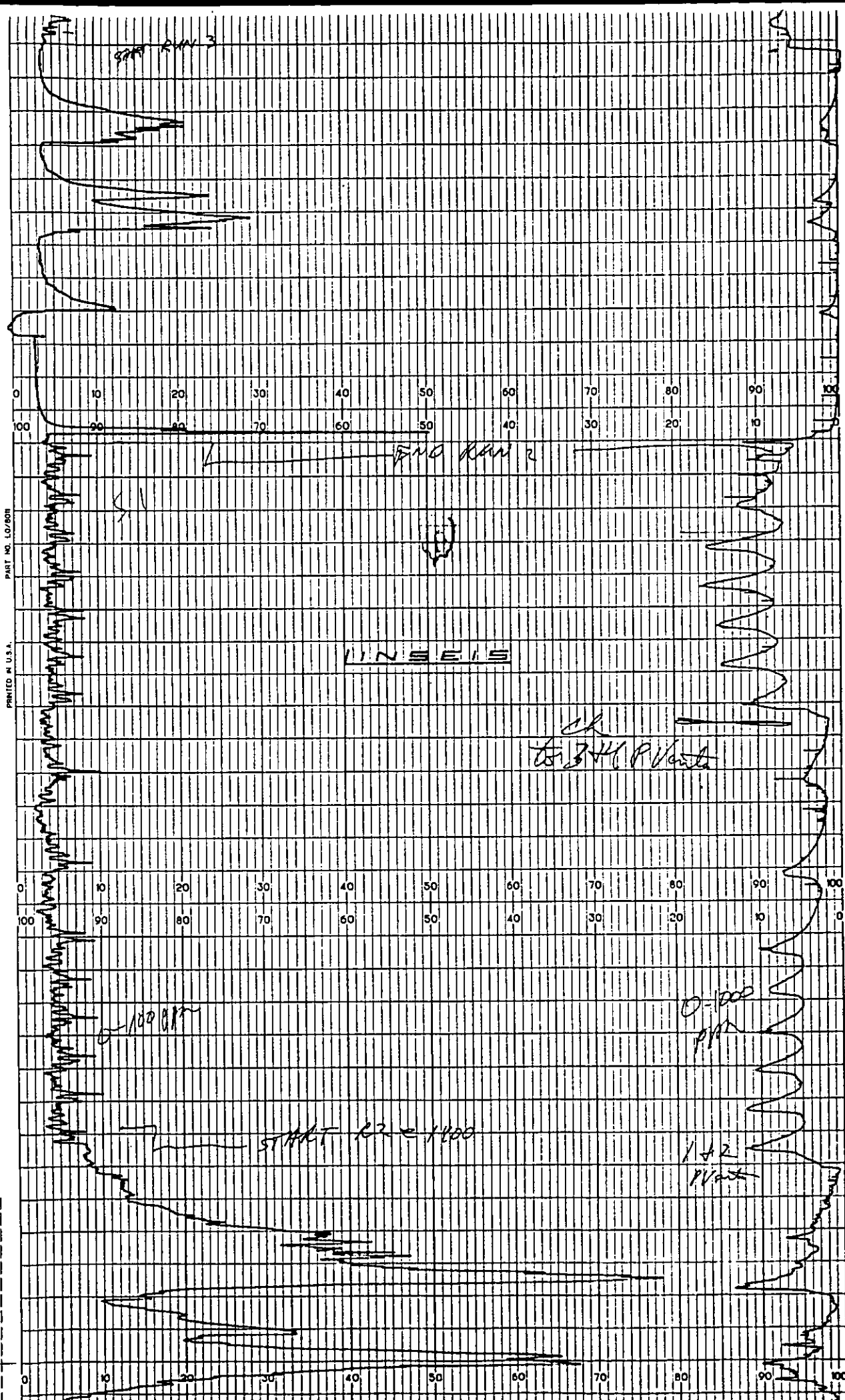
0-100
PVA

1+2
PVA

INSEIS

CR
to 344 PVA
0-100
PVA
1+2
PVA

PART NO. LO/808
PRINTED IN U.S.A.



START RAN 3

END RAN 2

LINE 15

CH
to 341 P.Venta

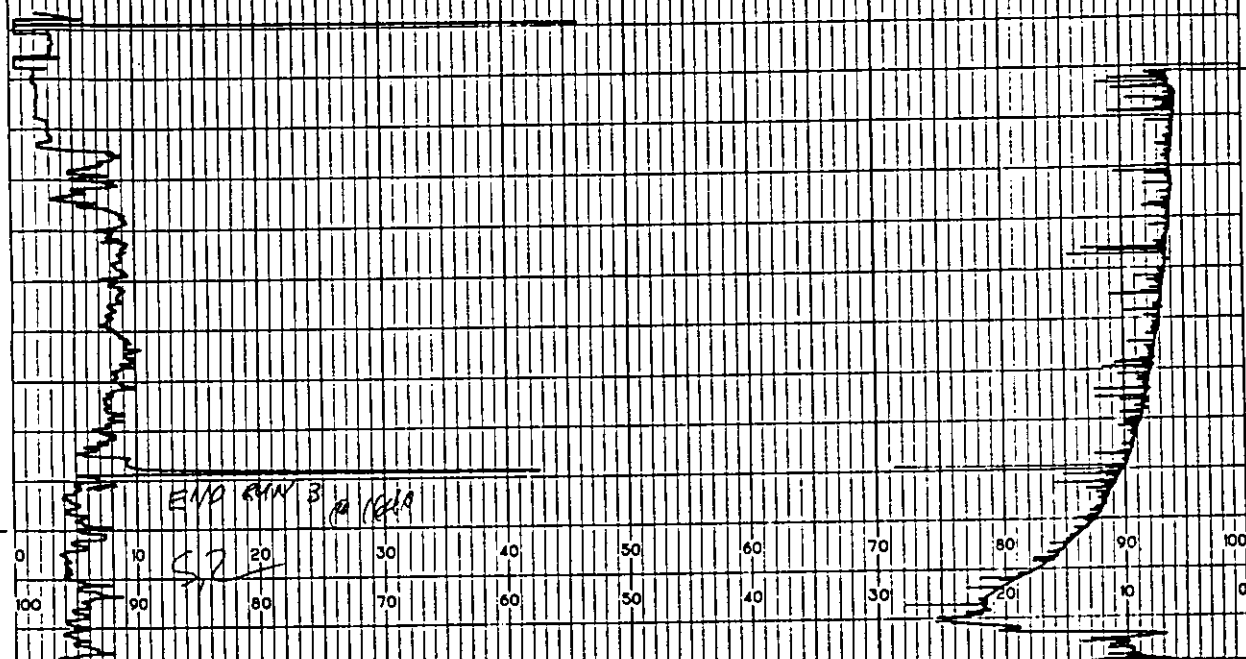
0-1000 P.V.A

START R2 @ 1400

0-1000
P.V.A

1/2
P.V.A

0 10 20 30 40 50 60 70 80 90 100
100 90 80 70 60 50 40 30 20 10 0



PART NO. LO/601

PRINTED IN U.S.A.

LINE 15

filter plugged

0 10 20 30 40 50 60 70 80 90 100
100 90 80 70 60 50 40 30 20 10 0

END RUN 3

SILSBEE TEXAS OSB STACK TEST OPERATIONAL SUMMARY

07/11/95

PRODUCTION PRESS

Press	420 - 440
Temp. (°F)	
Thickness (in)	0.438 & 0.719*
Density (nominal, lbs/cu ft)	41

<u>PRODUCTION</u> (Finished 3/8 in basis)	40,920 ft ² /hr **
	52,378 lbs/hr

*Nominal Thickness = 7/16 and 23/32 inch

**Annualized Production of 358,459,200 ft² 3/8 basis (8760 hrs)

SILSBEE TEXAS OSB STACK TEST OPERATIONAL SUMMARY

07/12/95

PRODUCTION PRESS

Press	420 - 440
Temp. (°F)	
Thickness (in)	0.438*
Density (nominal, lbs/cu ft)	41

<u>PRODUCTION</u> (Finished 3/8 in basis)	42,336 ft ² /hr**
	54,190 lbs/hr

*Nominal Thickness = 7/16 inch

**Annualized Production of 370,863,360 ft² 3/8 basis (8760 hrs)

SILSBEE TEXAS OSB STACK TEST OPERATIONAL SUMMARY

07/13/95

PRODUCTION PRESS

Press	420 - 440
Temp. (°F)	
Thickness (in)	0.438 & 0.469*
Density (nominal, lbs/cu ft)	41

<u>PRODUCTION</u> (Finished 3/8 in basis)	40,320 ft ² /hr **
	51,610 lbs/hr

*Nominal Thickness = 7/16 and 15/32 inch

**Annualized Production of 353,203,200 ft² 3/8 basis (8760 hrs)

SILSBEE TEXAS OSB STACK TEST OPERATIONAL SUMMARY

07/14/95

PRODUCTION PRESS

Press	420 - 440
Temp. (°F)	
Thickness (in)	0.438 & 0.250*
Density (nominal, lbs/cu ft)	41

PRODUCTION (Finished 3/8 in basis)

34,576 ft²/hr **
44,257 lbs/hr

*Nominal Thickness = 7/16 and 1/4 inch

**Annualized Production of 302,885,760 ft² 3/8 basis (8760 hrs)

**EMMISSIONS TESTING
SILSBEE OSB
JULY 11, 1995**

DRYER THROUGHPUT SUMMARY

TEST # 1

EMPTY WEIGHT: 13280 LBS.

DRIER #	WOOD FUEL	INLET TEMP	OUTLET TEMP	BIN BOTTOM	OUTLET MOISTURE	INLET MOISTURE	SCREENER TEMPERATURE	DURATION	FULL WEIGHT	LBS. PER HOUR
1	2762.16 lbs.	1103.6 degrees F	215.6 degrees F	33	5.6 %	49 %	135 degrees F	2 min.	14000 lbs.	21600 lbs.
2	2911.1 lbs.	1101.0 degrees F	213.6 degrees F	34	5.0 %	49 %	155 degrees F	2 min.	13920 lbs.	19200 lbs.
3	2484.59 lbs.	1015.6 degrees F	211.4 degrees F	33	5.9 %	49 %	121 degrees F	2 min.	13940 lbs.	19800 lbs.
5	2660.61 lbs.	1021.6 degrees F	208.2 degrees F	33	5.6 %	49 %	137 degrees F	2 min.	13940 lbs.	19800 lbs.

TEST # 2

EMPTY WEIGHT: 13280 LBS.

DRIER #	WOOD FUEL	INLET TEMP	OUTLET TEMP	BIN BOTTOM	OUTLET MOISTURE	INLET MOISTURE	SCREENER TEMPERATURE	DURATION	FULL WEIGHT	LBS. PER HOUR
1	2694.46 lbs.	1053.8 degrees F	213.4 degrees F	33	5.9 %	48 %	148 degrees F	2 min.	13980 lbs.	21000 lbs.
2	2708 lbs.	1040.2 degrees F	198.6 degrees F	34	5.4 %	48 %	151 degrees F	2 min.	13880 lbs.	21000 lbs.
3	2430.43 lbs.	1097.4 degrees F	224.8 degrees F	33	4.4 %	48 %	178 degrees F	2 min.	13860 lbs.	17400 lbs.
5	2531.98 lbs.	1037.6 degrees F	208.8 degrees F	33	9.6 %	48 %	144 degrees F	2 min. 33sec.	14140 lbs.	22145 lbs.

TEST # 3

EMPTY WEIGHT: 13240 LBS.

DRIER #	WOOD FUEL	INLET TEMP	OUTLET TEMP	BIN BOTTOM	OUTLET MOISTURE	INLET MOISTURE	SCREENER TEMPERATURE	DURATION	FULL WEIGHT	LBS. PER HOUR
1	2741.85 lbs.	1022.2 degrees F	212.8 degrees F	33	5.9 %	57 %	136 degrees F	2 min.	13960 lbs.	21600 lbs.
2	2768.93 lbs.	1007.4 degrees F	197.2 degrees F	34	4.9 %	57 %	143 degrees F	2 min.	13900 lbs.	19800 lbs.
3	2044.54 lbs.	946.6 degrees F	210.8 degrees F	33	5.9 %	49 %	160 degrees F	2 min.	13960 lbs.	21600 lbs.
5	2599.68 lbs.	1019.6 degrees F	206.6 degrees F	33	7.8 %	49 %	138 degrees F	2 min.	13840 lbs.	18000 lbs.

**EMMISSIONS TESTING
SILSBEE OSB
JULY 12, 1995**

DRYER THROUGHPUT SUMMARY

TEST # 2

EMPTY WEIGHT: 13220 LBS.

DRIER #	WOOD FUEL	INLET TEMP	OUTLET TEMP	BIN BOTTOM	OUTLET MOISTURE	INLET MOISTURE	SCREENER TEMPERATURE	DURATION	FULL WEIGHT	LBS. PER HOUR
1	2762.16 lbs.	1029.0 degrees F	212.8 degrees F	33	6.8 %	52 %	125 degrees F	2 min.	13940 lbs.	21600 lbs.
2	2376.27 lbs.	877.6 degrees F	196.4 degrees F	33	5.8 %	52 %	131 degrees F	2 min.	13900 lbs.	20400 lbs.
3	2125.78 lbs.	1017.8 degrees F	206.2 degrees F	33	7.1 %	46.3 %	128 degrees F	2 min.	13820 lbs.	18000 lbs.
5	2775.70 lbs.	994.6 degrees F	203.4 degrees F	33	12.6 %	16.3 %	113 degrees F	2 min.	13820 lbs.	18000 lbs.

TEST # 3

EMPTY WEIGHT: 13220 LBS.

DRIER #	WOOD FUEL	INLET TEMP	OUTLET TEMP	BIN BOTTOM	OUTLET MOISTURE	INLET MOISTURE	SCREENER TEMPERATURE	DURATION	FULL WEIGHT	LBS. PER HOUR
1	2897.56 lbs.	1084.0 degrees F	208.4 degrees F	33	9.3 %	47 %	113 degrees F	2 min.	13940 lbs.	21600 lbs.
2	2538.75 lbs.	912.4 degrees F	194.8 degrees F	33	6.3 %	47 %	127 degrees F	2 min.	13880 lbs.	19800 lbs.
3	2098.70 lbs.	952.4 degrees F	206.4 degrees F	33	7.2 %	50 %	124 degrees F	2 min.	13880 lbs.	19800 lbs.
5	2674.15 lbs.	999.6 degrees F	208.6 degrees F	33	6.5 %	50 %	127 degrees F	2 min.	13820 lbs.	18000 lbs.