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VOLATILE ORGANIC COMPOUND
AND
PARTICULATE EMISSION TESTING
AT
LOUISIANA-PACIFIC CORPORATION
HOULTON, MAINE

APCC AIR POLLUTION
CHARACTERIZATION
AND CONTROL, LTD.



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HOULTON, MAINE**

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EXECUTIVE SUMMARY

Air Pollution Characterization and Control, Ltd. (APCC) was retained by Louisiana-Pacific Corporation (Louisiana-Pacific) to provide Emissions Testing and Air Quality Engineering Services at their Houlton, Maine facility. The purpose of this project was to perform source emission measurements in order to calculate the VOC emissions and capture and control efficiency (CE). In addition, particulate matter (PM) emissions were determined in accordance with EPA Method 5 and NSPS Test Method 202 for front half PM (Method 5) and filterable PM including organic and inorganic condensables (Method 202). The testing was completed at the inlet (outlets of the surface and core dryer's primary cyclones) and outlet (stack) of the regenerative thermal oxidizer (RTO) for the following pollutants and diluents:

Particulate	RTO Stack
VOC	RTO Stack, Surface & Core Dryers
O ₂ and CO ₂	RTO Stack

The table below is a summary of the PM emissions test program which shows compliance with the Maine Department of Environmental Protection (ME DEP) permitted PM emission standard of 0.02 gr/dscf and 15.66 lb/hr from the combined dryer sources while operating at a rate sufficient to maintain press production within 90% of the maximum rate of 21.6 tph.

PARTICULATE EMISSION TESTING Louisiana-Pacific Corporation 9 July 1996

	AVERAGE EMISSIONS	EMISSIONS STANDARD
RTO Stack M-5	0.3 lb/hr	15.66 lb/hr
RTO Stack M-202	4.46 lb/hr*	15.66 lb/hr
RTO Stack M-5 & 202	4.64 lb/hr*	15.66 lb/hr

Note: * = Average includes only test Runs 2 and 3. See Section 2.1 for discussion.

The table below is a summary of the Volatile Organic Compound (VOC) emissions test program for the RTO Stack which shows compliance with the ME DEP VOC emission standard of 5.61 lb/hr and 95% capture and control efficiency (CE).

VOC EMISSION TESTING ON THE RTO STACK

	AVERAGE EMISSIONS	EMISSIONS STANDARD
RTO Stack	0.95 lb/hr	5.61 lb/hr
RTO CE	96.1%	95%

1.0 INTRODUCTION

Air Pollution Characterization and Control, Ltd. (APCC) was retained by Louisiana-Pacific Corporation (Louisiana-Pacific) to provide Emissions Testing and Air Quality Engineering Services at their Houlton, Maine facility. The purpose of this project was to perform source emission measurements in order to calculate the VOC emissions and capture and control efficiency (CE) as well as the particulate matter (PM) emission rate. Volatile Organic Compound (VOC) testing was performed in accordance with EPA Method 25A to demonstrate compliance with the standards for VOC emissions at the facility. Additionally, APCC performed testing to demonstrate compliance with the particulate matter (PM) standard in accordance with EPA Method 5 and NSPS Test Method 202 for front half PM (Method 5) and filterable PM including organic and inorganic condensables (Method 202) for the RTO stack.

This report prepared by APCC details the methodology that APCC used to determine compliance with the permitted standards for VOC and particulate matter.

This test program was performed on 9 July 1996 by Bruce A. Henning Principal Scientist at APCC, who served as the Project Engineer and a staff of APCC Engineers and Environmental Technicians. Process operations and site coordination was supplied by Mark Stile, Environmental Manager of Louisiana-Pacific.

Section 2 of this report presents the results and discussion and Section 3 contains a process description of the facility including the process data recorded during the test program. Section 4 details the test methods used during the test program. Section 5 contains APCC's quality assurance/quality control guidelines as implemented for this test program.

2.0 RESULTS AND DISCUSSION

This section details the results and discussion of the compliance program with regards to the compliance with the permitted standards for VOC and PM. The results are discussed as applicable to both the ME DEP Air Emissions License No. A-327-72-G-M and the US EPA Clean Air Act Consent Decree entered into with Louisiana-Pacific on 30 September 1993.

2.1 RTO Stack Particulate Matter Emissions

Compliance PM emissions testing was performed at the Louisiana-Pacific facility located in Houlton, Maine on 9 July 1996. Sampling was performed at the exhaust stack of the RTO. Testing was performed to determine emission concentrations and the emission rates in accordance with EPA Method 5 and NSPS Test Method 202 for front half particulate matter (Method 5) and filterable particulate matter including organic and inorganic condensables (Method 202).

Louisiana-Pacific's Air Emissions License No. A-327-72-G-M requires that the filterable (front half) emissions from the RTO stack be less than 0.02 gr/dscf and 15.66 lb/hr. The PM testing program was completed with both the surface and core dryer units operating at a rate sufficient to maintain press production within 90% of the maximum rate of 21.6 tph. The emission rate was determined to be in compliance at 5.4% of the allowable 15.66 lb/hr with a total emission rate of 0.30 lb/hr and a PM concentration of 5.43E-04 gr/dscf. A summary of each of the PM test results based on the filterable (front half) emissions from the RTO stack is presented below in summary Table 2-1.

Table 2-1
Data Summary for Method 5 PM on the RTO Stack

Louisiana-Pacific
Houlton, Maine

TEST NUMBER: DATE: TIME:		1 7/9/96 1515-1615	2 7/9/96 1730-1900	3 7/9/96 1955-2055	
PROCESS CONDITIONS	UNITS				AVERAGE
Press Production Rate	tph	19.4	19.4	19.4	19.4
SAMPLE CONDITIONS					
Meter Volume	dscf	41.1	42.6	42.6	42.1
Isokinesis	%	95.3	98.1	99.7	97.7
Filterable Particulate Catch	mg	2.6	1.0	0.8	1.5
STACK CONDITIONS					
Stack Gas Flowrate	dscf/min	63,946	64,445	63,461	63,951
Average Stack Temperature	°F	258	257	256	257
Water Vapor in Stack Gas	% v/v	23.0	22.8	23.2	23.0
CO ₂ in Stack Gas	%	3.7	5.9	4.5	4.7
O ₂ in Stack Gas	%	16.5	16.1	15.9	16.0
MEASURED EMISSIONS					
Particulate Concentration	gr/dscf	9.77E-04	3.62E-04	2.90E-04	5.43E-04
Mass Emission Rate	lb/hr	0.54	0.20	0.16	0.30

Revised 8/30/96

Three 60-minute tests were performed on 9 July 1996 to determine emission concentrations of PM under press operating conditions which yielded 19.43 tons per hour or 90% of the maximum operating capacity. The emission concentration in grain per dry standard cubic feet (gr/dscf) averaged $5.43\text{E-}04$ gr/dscf, below the 0.02 gr/dscf emission standard. The results for the three tests were 0.54, 0.20, and 0.16, pounds per hour (lb/hr) respectively. The average of the three tests was calculated to be 0.30 lb/hr. This represents 5.4 % of the total allowed emission rate of 15.66 lb/hr.

The oxygen levels varied from 3.7 % to 5.9 % for all three of the tests. Oxygen concentrations averaged 4.7 % for the entire test program. Emissions data summaries and copies of the Method 5 sheets as recorded during the test program are presented in Appendix C.

All three tests performed were within the $100\% \pm 10\%$ isokinetic acceptable range as required by the reference method. Both the sampling and pitot leak checks were acceptable at less than 0.02 cfm.

The US EPA Clean Air Act Consent Decree entered into with Louisiana-Pacific on 30 September 1993 requires that the results be reported as total PM. Total PM was determined to have an emission rate of 4.64 lb/hr and a PM concentration of $8.47\text{E-}03$ gr/dscf based on the average of Test Runs 2 and 3. Test Run 1 was discarded due to contamination as described below.

As seen in the tables below, Test Run 1 seems to be an outlier in the fact that total PM results are 4 times the average of Test Runs 2 and 3. The Run 1 condensable sample underwent further analysis by infrared (IR) scan to determine that silicone lubricant contamination contributed to the high results. Therefore, Run 1 is not included in the average reported CPM results. The Interpoll Laboratory's analytical data is presented in Appendix G.

A summary of each of the additional condensable PM results is presented in Tables 2-2 and 2-3. All associated field data and detailed summaries are presented in Appendix B of this report.

2.2 VOC Emissions and RTO Capture Efficiencies

This section presents a discussion of test data collected during each VOC emission test. APCC performed three 60 minute tests on the RTO stack and the outlets from the surface and core dryer primary cyclones which served as the inlets to the RTO for the calculation of the RTO's CE. These tests were performed at the same time as the PM tests under the same operating conditions as described above, detailed in Section 3 and presented in Appendix E, pages 2 and 3. A results summary for each test run is presented in Table 2-4. Complete tabulated data for each test is presented in Appendix B.

Table 2-2
Data Summary for Filterable PM Containing Organic Condensables
Louisiana-Pacific
Houlton, Maine

TEST NUMBER:		1	2	3	
DATE:		7/9/96	7/9/96	7/9/96	
TIME:		1515-1615	1730-1900	1955-2055	
PROCESS CONDITIONS	UNITS				AVERAGE
Press Production Rate	tph	19.4	19.4	19.4	19.4
SAMPLE CONDITIONS					
Meter Volume	dscf	41.1	42.6	42.6	42.6
Isokinesis	%	95.3	98.1	99.7	98.9
Condensable PM Catch	mg	92.0	23.0	22.0	22.5
STACK CONDITIONS					
Stack Gas Flowrate	dscf/min	63,946	64,445	63,461	63,953
Average Stack Temperature	°F	258	257	256	257
Water Vapor in Stack Gas	% v/v	23.0	22.8	23.2	23.0
CO ₂ in Stack Gas	%	3.7	5.9	4.5	5.2
O ₂ in Stack Gas	%	16.5	16.1	15.9	16.0
MEASURED EMISSIONS					
Particulate Concentration	gr/dscf	3.46E-02	8.33E-03	7.96E-03	8.15E-03
Mass Emission Rate	lb/hr	18.93	4.60	4.33	4.46

Note: Average includes only test Runs 2 and 3. See Section 2.1 for details.

Table 2-3
Data Summary for Total PM (M-5 & 202)
Louisiana-Pacific
Houlton, Maine

TEST NUMBER:		1	2	3	
DATE:		7/9/96	7/9/96	7/9/96	
TIME:		1515-1615	1730-1900	1955-2055	
PROCESS CONDITIONS	UNITS				AVERAGE
Press Production Rate	tph	19.4	19.4	19.4	19.4
SAMPLE CONDITIONS					
Meter Volume	dscf	41.1	42.6	42.6	42.6
Isokinesis	%	95.3	98.1	99.7	98.9
Total Particulate Catch	mg	94.6	24.0	22.8	22.5
STACK CONDITIONS					
Stack Gas Flowrate	dscf/min	63,946	64,445	63,461	63,953
Average Stack Temperature	°F	258	257	256	257
Water Vapor in Stack Gas	% v/v	23.0	22.8	23.2	23.0
CO ₂ in Stack Gas	%	3.7	5.9	4.5	5.2
O ₂ in Stack Gas	%	16.5	16.1	15.9	16.0
MEASURED EMISSIONS					
Particulate Concentration	gr/dscf	3.55E-02	8.69E-03	8.25E-03	8.47E-03
Mass Emission Rate	lb/hr	19.47	4.80	4.49	4.64

Note: Average includes only test Runs 2 and 3. See Section 2.1 for details.

Table 2-4

Data Summary for VOC Emissions and CE
Louisiana-Pacific, Houlton, Maine

	INLET SITE 1 lbs/hr	EMISSION RATES INLET SITE 2 lbs/hr	INLET 1 & 2 lbs/hr	OUTLET SITE 4 lbs/hr*	CAPTURE EFFICIENCY (CE) %
Test 1 Average	9.7	15.6	25.3	0.7	97.4
Test 2 Average	9.2	13.1	22.4	1.5	93.4
Test 3 Average	10.9	16.5	27.4	0.7	97.5
TEST PROGRAM AVERAGES			25.0	0.9	96.1
VOC Limit = 5.61 lbs/hr*					

The average test program VOC emission rate at the RTO stack outlet was determined to be 0.9 lb/hr, which is 16% of the ME DEP permitted emission standard of 5.61 lb/hr. The VOC concentrations at the RTO stack ranged from 0.4 ppm to 18.2 ppm, while the test program average was 4.6 ppm.

The following equation was used to calculate VOC lbs/hr emissions.

$$\text{lbs/hr} = (\text{ppm}) * (\text{Conversion Factor}) * (Q_s, \text{ scfm}) * (60 \text{ min. /hr})$$

where: Conversion Factor = THC as methane = 4.149E-08
 Q_s = standard flow, scf/min

The sum of the results from Sites 1 and 2, after the primary cyclones were used to determine the VOC contribution from the dryers. The CE of the pollution control system, the RTO was calculated as follows:

$$\text{VOC EFFICIENCY} = 1 - ((\text{VOC @ Site 4}) / (\text{VOC @ Site 1} + \text{VOC @ Site 2})) * 100$$

As can be seen from the table presented above the test program average CE was calculated to be 96.1%. The three test averages were 97.4, 93.4, and 97.5 % for tests 1, 2, and 3 respectively.

3.0 PROCESS AND OPERATIONS

The Louisiana-Pacific facility in Houlton Maine is an oriented strand board manufacturing facility that produces structural panel used for various construction applications. The facility is identified by the Standard Industrial Classification Code 2493. A complete process flow diagram is presented in Appendix A.

The plant purchases logs that are debarked and fed to a waferizer. The bark is used for fuel in the thermal oil heater. The waferizer flakes the logs into thin pieces, which are approximately three inches long by one inch wide by 1/32 inch thick. The freshly cut pieces have a moisture content of approximately 50%. The wet flakes go through a rotary dryer which reduces the moisture content to between four and eight percent. The flakes are then captured by the primary cyclone and the exhaust gas passes through a wet electrostatic precipitator (ESP) followed by a regenerative thermal oxidizer (RTO).

The flakes collected by the primary cyclone drop into a rotary screen, which separates the correctly sized flakes for further processing. The material passing through the screen is used as fuel in the dryer. Wax and resin are mixed with the flakes in rotary blenders. Formers then evenly distribute the flakes onto a moving conveyer. A separate former is used to orient the bottom, core and top layers of the board. The continuous mat of flakes is separated into press size segments by the flying cut-off saw.

The loader loads the boards into the press and with the combination of heat (supplied by the thermal oil heater) and pressure, the wafer mats are turned into solid boards. These boards are unloaded and cut by the trim saw to the desired sizes. The dust formed by this operation is collected and used as fuel in the wafer dryer.

The facility operates several pollution control devices to control emissions. As mentioned above, the rotary dryer exhaust is controlled by a wet ESP and the RTO. Emissions generated by the thermal oil heater pass through a cyclone and ESP. Emissions from the board press are controlled by a RTO.

3.1 Process Equipment Description and Operating Conditions

The description of the process equipment that was tested is two MEC model 1248 T triple pass rotary drum wafer dryers with rated capacities of 230 tons per hour (tph) of wafers at six percent moisture. The primary burners are McConnell model 48 wood fired cyclonic suspension burners with rated capacities of 40 MM Btu/hr.

The dryers were operated at a rate sufficient to maintain press production within 90% of the maximum rate of 21.6 tph of finished product. The actual press production rate was maintained at 90 % with a rate of 19.4 tph.

The dryers' McConnell burners used dry fines as fuel during the testing. The fuel counts were recorded during the test program and are presented in Appendix E. The counts were factored based on the current quarterly fuel calibration to obtain the pounds of fuel burned. Wafers were dried to 4.5% - 5.5% moisture by weight. The

dryer operating parameters were recorded at ten minute intervals and are presented in detail in Appendix D. Dryer production rate in pounds of dry furnish per hour was determined based on the press production plus screened fines and board trim using the following formula:

$$\text{lb Dryer Production/Hr} = \frac{(\text{Tons press production/Hr}) / 2000}{1 - (0.07 + 0.08)}$$

where: Board trim = 7 % of finished product weight
screened fines = 8 % of finished product weight

3.2 Control Equipment Description and Operating Conditions

Emissions from the dryers are controlled by a wet electrostatic precipitator (ESP) manufactured by Geoenergy model 1013-378 2 T/R GEOENERGY E-Tube® followed by a Wheelabrator Clean Air Systems Inc. model No. 9220-7-95-04/96 regenerative thermal oxidizer (RTO). Operating specifications of the wet ESP include:

- Primary and secondary volts > 40 KV;
- Primary and secondary amperes 150-300 mA;
- Number of fields on line: 2;
- Flue gas conditioning: Saturation of gas stream; and
- Voltages, amperes flush cycles, and blowdown information.

Operating specifications of the RTO include:

- Combustion temperature: >1500 °F; and
- Primary fuel: Propane.

The test program averages are presented in Table 3-1 and further detailed in Appendix E, pages 2 and 3.

Table 3-1
Process Data Summary
Louisiana-Pacific, Houlton, Maine

PROCESS CONDITION	UNITS	PROGRAM AVERAGE
Press Production Rate	tph	19.43
Dryers' Production Rate	lb/hr	44,597
Total Fuel Burned	tph	2.87
Incoming Moisture	%	33.05
Dry Moisture	%	6.17
Inlet Temperature	°F	1,168
RTO Temperature No. 1	°F	1,507
RTO Temperature No. 2	°F	1,510
RTO Temperature No. 3	°F	1,510

4.0 SAMPLING AND ANALYTICAL METHODOLOGY

APCC mobilized two Environmental Monitoring Laboratories (EML) and other test equipment at the test site. Upon arrival, APCC met with the project management supervisor and site coordinator familiarizing themselves with the facility, safety procedures, and process operations. The following sections present brief descriptions of the sampling and analytical methodologies.

4.1 Continuous Emission Monitoring

APCC performed continuous emission monitoring to determine emissions of carbon dioxide (CO₂), oxygen (O₂), and Volatile Organic Compounds (VOC) in accordance with EPA Methods 3A and 25A. All CEM data was recorded using Tracor/Westronics 3000 automatic digital data loggers. Copies of the strip chart recordings are presented in Appendix D.

The CEM systems housed in the APCC EMLs were located at the base of the RTO stack and below Sites 1 and 2. In each system stack gas was drawn through an in-stack filter, a heated stainless steel heated probe, heated Teflon sample line (320°F nominal), the VOC sample was drawn directly from the heated sample line into the VOC analyzer for analysis on a wet basis. A portion of the sample was split at the back of the VOC analyzer and drawn through a Peltier-type sample conditioner by a leakless Teflon diaphragm pump. The sample was then pumped through a manifold under slightly positive pressure with a bypass to atmosphere. CO₂ and O₂ samples were continuously drawn from this manifold to their respective analyzers. The VOC sample bypassed the condenser system and was passed directly to the analyzer. A schematic of the APCC's instrument reference method (IRM) monitoring systems is presented in the Figure 4-1.

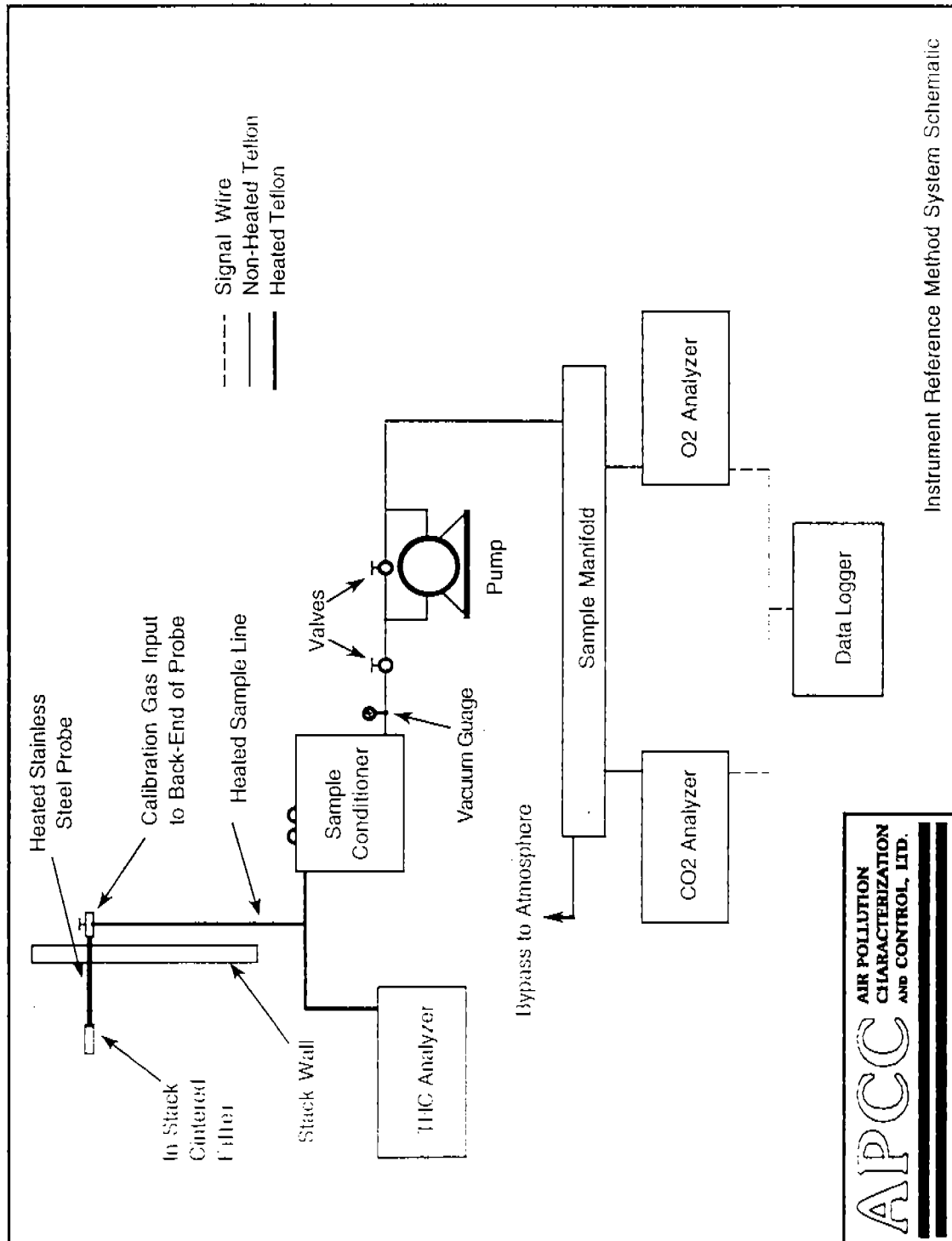
4.1.1 Volatile Organic Compound Analyzers

A VIG Industries dual channel total hydrocarbon analyzer, which utilizes two flame ionization detectors (FIDs) to measure, as methane, hydrocarbons C₁ through C₁₈; was used to sample from the outlets of Sites 1 and 2 the surface and core dryers simultaneously with the TECO Model 51 Total Hydrocarbon Analyzer. Approximately 5.0 lpm of sample gas is drawn from the sample locations through Teflon sample line heated to 350°F (nominal). The sample gas is drawn through a heated filter and valving by a heated pump. The sample gas then enters the heated detector bench which contains the FID.

4.1.2 Oxygen Analyzers

A Westinghouse/Maihak OXIGOR O₂ analyzer calibrated on the 0-25% scale was used to monitor concentrations of oxygen in the exhaust stream. This instrument utilizes the magnetic dumbbell sphere (paramagnetic) principle, which comparatively measures the magnetic susceptibility of a gas volume by the force acting upon a non-magnetic test body suspended in a disproportionate magnetic field. Output current is linearly proportional to the oxygen concentration.

Figure 4-1 APCC IRM System Schematic



A Teledyne 326RA series analyzer was also used in the other EML to monitor O₂ concentrations in a gas stream. This instrument utilizes a micro fuel cell to measure oxygen content. Output voltage is linearly proportional to the oxygen concentration in the sample stream. This analyzer was calibrated on the 0-25% scale.

4.1.3 Carbon Dioxide Analyzers

A Westinghouse/Maihak FINOR CO₂ analyzer was used to monitor carbon dioxide emissions in EML No. 1. This instrument operates on the principle of carbon dioxide having a known characteristic absorption spectra in the infrared range.

In addition, a Westinghouse Model UNOR 6N non-dispersive infrared gas analyzer was used to measure CO₂ concentrations. The analyzer operates on the measurement principle based on CO₂ having a known characteristic absorption spectra in the infrared range. It contains an infrared detector that uses the non-dispersive single beam technique with alternative modulation of the sample and reference cells. Radiation absorbed by CO₂ in the sample cell produces a capacitance change in the detector which is proportional to the CO₂ concentration. Both the CO₂ were calibrated on the 0-25% scale.

4.1.4 Calibration

Four point (zero, low, mid and span) calibrations for hydrocarbons and three point (zero, mid and span) calibrations for other parameters were performed on the analytical instrumentation at the beginning of the test program to establish instrument linearity. A zero and span calibration on each instrument was performed before and after each test. The system was also leak and bias checked prior to the test program. EPA Protocol 1 gases were used for all calibrations.

4.1.5 Data Acquisition and Handling

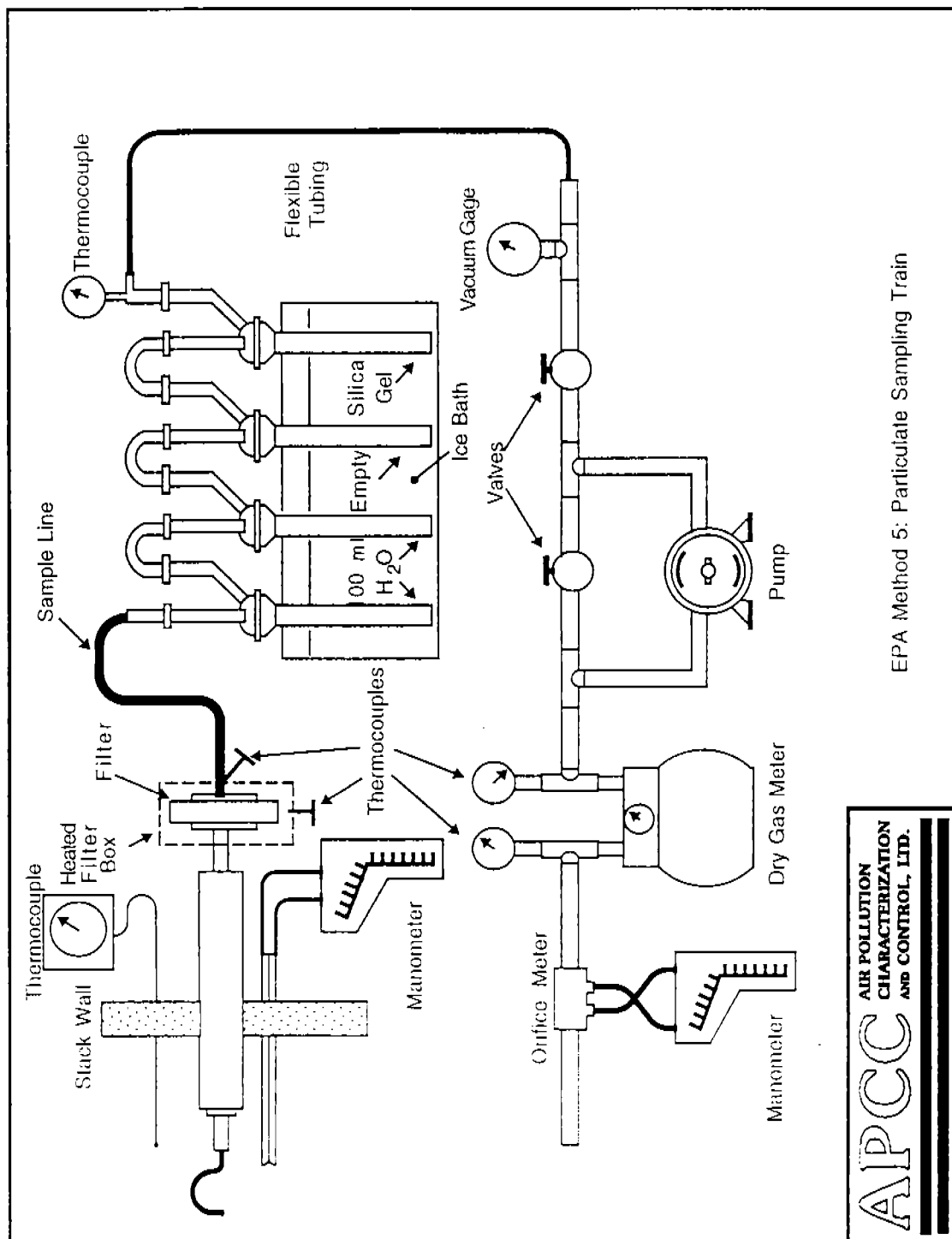
All CEM data was monitored by a Tracor/Westronics 3000 digital data loggers which recorded on a strip charts using its integral color printer. Trends were monitored using the strip chart mode with averages printed digitally for 10-minute intervals. Emission data are "viewed" by the data logger at 5-second intervals. This enables real-time emission data to be available on-site.

4.2 Particulate Emission Measurements

Particulate sampling was performed in accordance with EPA Method 5, as described in the July 1, 1995 edition of the *Code of Federal Regulations* (CFR). In addition, NSPS Test Method 202 for front half PM (Method 5) and filterable PM including organic condensable (Method 202) was completed. Triplicate 60-minute tests were performed at all three sites. However, for the purposes of this compliance report only the Site 4 PM data is reported.

A schematic of the sampling train similar to the one that was used during testing is presented in Figure 4-2. The RTO stack particulate sampling was performed in

Figure 4-2 EPA Method 5 Sampling Train



EPA Method 5: Particulate Sampling Train

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accordance with a EPA Method 5, as described in the July 1, 1995 edition of the *Code of Federal Regulations* (CFR). The particulate sampling train consisted of a nozzle attached to a glass-lined probe which is heated to prevent condensation. Whatman EPM 2000 fiberglass filter paper supported in a 4-1/2 inch glass filter holder was used as the collection media. The filter assembly will be enclosed in a heated box to maintain temperatures at $248^{\circ}\text{F} \pm 25^{\circ}\text{F}$. A thermocouple located inside the back half of the filter holder, was used to monitor the gas stream temperature and verify that the temperature is kept at $248^{\circ}\text{F} \pm 25^{\circ}\text{F}$.

An ice bath containing four impingers was attached to the back end of the filter via a flexible umbilical tube. The first, third, and fourth impingers were of modified Greenburg-Smith design, while the second will be the standard Greenburg-Smith design. The first two impingers contained 100 ml distilled water, the third is dry, and the fourth contains 200 grams of indicating silica gel to remove any remaining moisture. Flexible tubing, vacuum gauge, needle valves, leakless vacuum pump, bypass valve, dry gas meter, calibration orifice and inclined manometer complete the sampling train. The stack velocity pressure was measured using a pitot tube and inclined manometer in accordance with EPA Method 2. The stack temperature was monitored using a calibrated K-type thermocouple connected to a potentiometer.

A nomograph was used to quickly determine the orifice pressure drop required for a pitot velocity pressure and stack temperature in order to maintain isokinetic sampling conditions. Sampling flow was adjusted by means of the bypass valve. Before and after each particulate test run, the sampling train was leak checked and acceptable at less than 0.02 cubic feet per minute (cfm). The moisture content of the exhaust gases was determined during each test in accordance with EPA Method 4. Test data was recorded on field data sheets as presented in Appendix C of this report.

Sample Recovery:

At the end of each test, three sample containers were used as follows:

- | | |
|-----------------|--|
| Container No. 1 | Filter |
| Container No. 2 | Acetone wash of probe and front half of filter. The probe and nozzle will be washed and brushed three times. |
| Container No. 3 | Silica gel from the fourth impinger. |

Sample Analysis:

The samples were transported to the laboratory and the following analyses performed:

- | | |
|-----------------|---|
| Container No. 1 | Transfer the filter and any loose particulate matter from the sample container into a desiccator and dry for approximately 24 hours. The sample is then weighed to a constant weight. Reported results to the nearest 0.1 mg. |
|-----------------|---|

- Container No. 2 The acetone washing will be transferred to a tared beaker and evaporated to dryness. Desiccated and dried to a constant weight. Reported results to the nearest 0.1 mg.
- Container No. 3 Silica gel will be weighed to the nearest 0.5 g. The weight of the moisture entrapped in the silica gel, along with the volume of moisture which condensed in the impingers, will be used to calculate the moisture content of the flue gas.

A computer program developed for the Macintosh was used to calculate emission rates in grains per dry standard cubic foot (gr/dscf) and pounds per hour (lb/hr). The program was also calculate percent moisture, molecular weight of the stack gas at stack conditions, and the percent isokinesis.

4.3 Volumetric Flow Rate Determination and Sampling Locations

Exhaust gas volumetric flow rate was determined at the inlets and outlet of the RTO in conjunction with each of the VOC emission tests in accordance with EPA Methods 1 and 2 which were performed in conjunction with the PM tests completed at all three locations.

Two sample ports at Site 1 are located at 90° of one another in the exhaust from the surface dryer 25 ft or 7.1 diameters upstream and 45 ft or 12.6 diameters downstream from the nearest respective flow disturbances in the 42 inch diameter duct.

Two sample ports at 90° of one another in the 42 inch diameter core dryer duct at Site 2 are located at 29 ft or 8.3 diameters upstream and 29 ft or 8.3 diameters downstream from the nearest disturbances.

In accordance with EPA Method 1, 12 traverse points were measured at Sites 1 and 2 to determine stack gas velocity and temperature.

The RTO stack sampling location was on the platform at the 60 ft elevation. The two sampling ports are located in the 82 inch stack at 36 ft or 5.3 diameters upstream and 40 ft or 5.6 diameters downstream from the nearest disturbances. Therefore, in accordance with EPA Method 1, 20 traverse points were measured to determine stack gas velocity and temperature.

Appendix A presents diagrams of each sampling location. Appendix C details the velocity and Method 5 traverse points used at each sampling location.

5.0 QUALITY ASSURANCE

The project manager is responsible for implementation of the quality assurance program as applied to the project.

5.1 Sampling Quality Assurance

Generally, implementation of quality assurance procedures for source measurement programs is designed so that the work is done:

1. By competent, trained individuals experienced in the specific methodologies being used.
2. Using properly calibrated equipment.
3. Using approved procedures for sample handling and documentation.

Measurement devices, pitot tubes, dry gas meters, thermocouples, etc. are uniquely identified and calibrated with documented procedures and acceptance criteria before and after each field effort. Records of all calibration data are maintained in the files.

Data are recorded on standard forms. Bound field notebooks are used to record observations and miscellaneous elements affecting data, calculations, or evaluation.

Specific details of APCC's QA program for stationary air pollution sources may be found in "Quality Assurance Handbook for Air Pollution Measurement Systems", Volume III (EPA-600/4-7-027b).

5.2 Equipment Calibration

The CEM system was calibrated at the beginning and end of each test day as well as leak and biased checked before and after each test. All calibration gases were EPA Protocol 1. Multi-point calibrations were performed to established linearity prior to sampling and throughout the test program. Appendix B presents the EML CEM work sheets which include all of the calibration data and bias corrections. All of the calibrations met the specifications of EPA Method 6C Section 8.

5.3 Data Reduction and Reporting

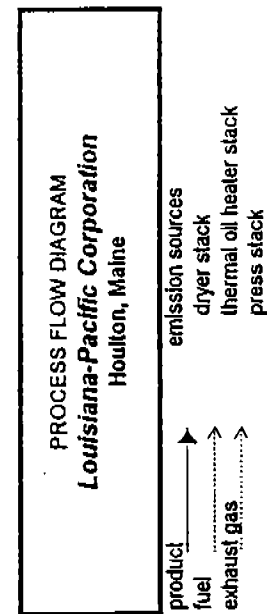
The Project Engineer developed a data reduction system to conform to the collection of field data to be reduced and quantitative results for the final report. The methods for data reduction were specified and presented to the Program Manager before the field effort. Raw data recorded on field data sheets, bound laboratory books, and data logger strip charts are presented in the Appendix of this report.

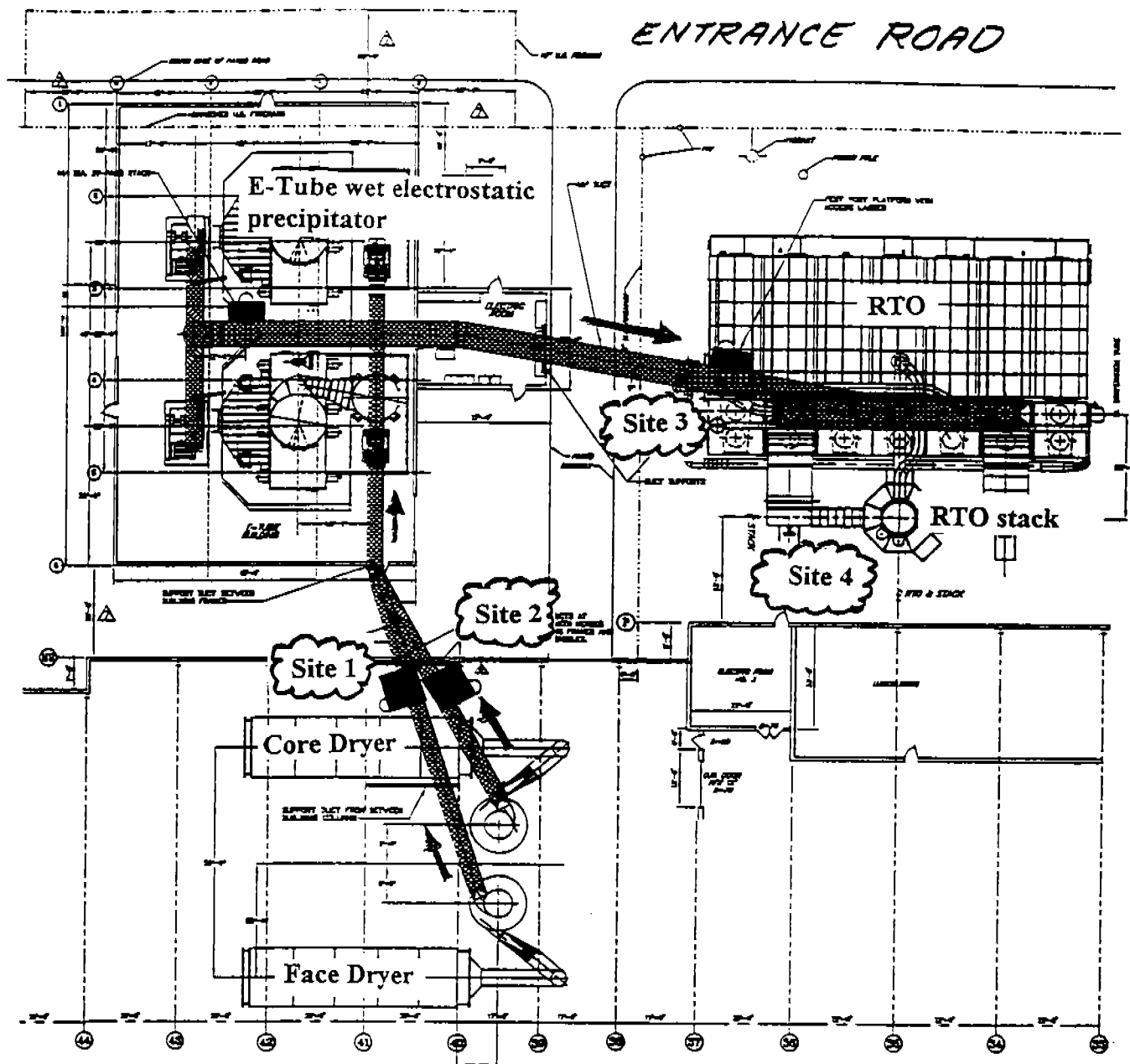
5.4 Data Validation

Validation of data were reviewed by the Manager of Engineering and Company President against the QA/QC criteria of the specific methods. The data were assessed to the quality and accuracy as required to meet the objectives of the sampling program. Hand calculations were performed with raw data separate from the reported calculations and results. All documentation was checked for correctness, completeness and verified as checked.

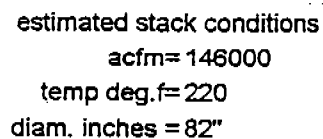
A data assessment of sampling results was also performed during scheduled time periods to ensure quality data is collected and processed. Corrective action was implemented if warranted to ensure QA/QC procedures are met. No corrective actions were necessary.

APPENDIX A
Process Flow Chart
&
Sampling Location Diagrams









APPENDIX B
Results Summaries

CLIENT:		LOUISIANA PACIFIC					
LOCATION:		SITE 4 (RTO STACK)					
PROJECT NUMBER:		96053					
TEST NUMBER:							
DATE:		1	2	3	AVERAGE		
TIME :		7/9/96	7/9/96	7/9/96			
		1515-1615	1730-1900	1955-2055			
TEST DATA INPUT							
Barometric Pressure	Pbar	in. Hg	29.88	29.88	29.88		
Stack Area	A	ft ²	36.7	36.7	36.7		
Nozzle Diameter (in.)	Dn	in.	0.275	0.275	0.275		
Total Sampling Time	Ø	min.	60	60	60		
Calibration Factor	Y	-	1	1	1		
Pitot Coefficient	Cp	-	0.84	0.84	0.84		
Average Square Root of Velocity Head	√ΔPavg	in. H ₂ O	0.753	0.76	0.749		
Average Orifice Pressure Drop	ΔH	in. H ₂ O	2.01	2.04	2		
Average Meter Temperature	Tm	°F	84	80	78		
Average Stack Pressure	Pg	in. H ₂ O	0.57	0.56	0.57		
Average Stack Temperature	Ts	°F	258	257	256		
Meter Volume @ Meter Conditions	Vm	ft ³	42.16	43.41	43.28		
Total Water Collected	Vlc	ml	261	267	274		
CO ₂ in Stack Gas	CO ₂	%	3.7	5.9	4.5		
O ₂ in Stack Gas	O ₂	%	16.5	16.1	15.9		
CO in Stack Gas	CO	%	0	0	0		
Total Filtered Particulate Catch	Pmt	mg	2.6	1.0	0.8	1.5	
CALCULATED VALUES							
Meter Volume	Vmstd	dscf	41.1	42.6	42.6	42.1	
Water Vapor in Stack Gas	Bws	%	23.03	22.78	23.23	23.01	
Molecular Weight of Stack Gas (dry)	Md	g/g-mole	29.3	29.6	29.4	29.4	
Molecular Weight of Stack Gas (wet)	Ms	g/g-mole	26.7	26.9	26.7	26.8	
Average Velocity of Stack Gas	Vs	ft/min	3,078	3,088	3,054	3,073	
Actual Stack Gas Flowrate	Q	acf/min	112,963	113,326	112,086	112,792	
Stack Gas Flowrate	Qsd	dscf/min	63,946	64,445	63,461	63,951	
Isokinetics	I	%	95.3	98.1	99.7	97.7	
EMISSION CONCENTRATION							
Particulate Emission Concentration	PCgr	gr/acf	7.18E-04	2.67E-04	2.14E-04	4.00E-04	
Particulate Emission Concentration	PCgrsd	gr/dscf	9.77E-04	3.62E-04	2.90E-04	5.43E-04	
Particulate Emission Concentration	PClbsd	lb/dscf	1.39E-07	5.17E-08	4.13E-08	7.75E-08	
Particulate Emission Concentration	PCµgm	µg/dscm	2237	829	663	1243	
EMISSION RATE							
Particulate Emission Rate	PER	lbs/hr	0.54	0.20	0.16	0.30	

CLIENT:		LOUISIANA PACIFIC					
LOCATION:		SITE 4 (RTO STACK)					
PROJECT NUMBER:		96053					
TEST NUMBER:			1	2	3	AVERAGE	
DATE:			7/9/96	7/9/96	7/9/96		
TIME :			1515-1615	1730-1900	1955-2055		
TEST DATA INPUT		SYMBOL	UNITS				
Barometric Pressure	Pbar	in. Hg	29.88	29.88	29.88		
Stack Area	A	ft2	36.7	36.7	36.7		
Nozzle Diameter (in.)	Dn	in.	0.275	0.275	0.275		
Total Sampling Time	Ø	min.	60	60	60		
Calibration Factor	Y	-	1	1	1		
Pitot Coefficient	Cp	-	0.84	0.84	0.84		
Average Square Root of Velocity Head	√ΔPavg	in. H2O	0.753	0.76	0.749		
Average Orifice Pressure Drop	ΔH	in. H2O	2.01	2.04	2		
Average Meter Temperature	Tm	°F	84	80	78		
Average Stack Pressure	Pg	in. H2O	0.57	0.56	0.57		
Average Stack Temperature	Ts	°F	258	257	256		
Meter Volume @ Meter Conditions	Vm	ft3	42.16	43.41	43.28		
Total Water Collected	Vlc	ml	261	267	274		
CO2 in Stack Gas	CO2	%	3.7	5.9	4.5		
O2 in Stack Gas	O2	%	16.5	16.1	15.9		
CO in Stack Gas	CO	%	0	0	0		
Total Condensible PM Catch	PMt	mg	92.0	23.0	22.0	22.5	
CALCULATED VALUES							
Meter Volume	Vmstd	dscf	41.1	42.6	42.6	42.6	
Water Vapor in Stack Gas	Bws	%	23.03	22.78	23.23	23.0	
Molecular Weight of Stack Gas (dry)	Md	g/g-mole	29.3	29.6	29.4	29.5	
Molecular Weight of Stack Gas (wet)	Ms	g/g-mole	26.7	26.9	26.7	26.8	
Average Velocity of Stack Gas	Vs	ft/min	3,078	3,088	3,054	3071.0	
Actual Stack Gas Flowrate	Q	acf/min	112,963	113,326	112,086	112706.2	
Stack Gas Flowrate	Qsd	dscf/min	63,946	64,445	63,461	63952.9	
Isokinetics	I	%	95.3	98.1	99.7	98.9	
EMISSION CONCENTRATION							
Particulate Emission Concentration	PCgr	gr/acf	2.54E-02	6.13E-03	5.87E-03	6.00E-03	
Particulate Emission Concentration	PCgrsd	gr/dscf	3.46E-02	8.33E-03	7.96E-03	8.15E-03	
Particulate Emission Concentration	PClbsd	lb/dscf	4.93E-06	1.19E-06	1.14E-06	1.16E-06	
Particulate Emission Concentration	PCµgm	µg/dscm	79161	19078	18237	18657.4	
EMISSION RATE							
Particulate Emission Rate	PER	lbs/hr	18.93	4.60	4.33	4.46	

NOTE: Average includes only Runs 2 and 3.

CLIENT:	LOUISIANA PACIFIC				
LOCATION:	SITE 4 (RTO STACK)				
PROJECT NUMBER:	96053				
TEST NUMBER:		1	2	3	AVERAGE
DATE:		7/9/96	7/9/96	7/9/96	
TIME :		1515-1615	1730-1900	1955-2055	

TEST DATA INPUT	SYMBOL	UNITS				
Barometric Pressure	Pbar	in. Hg	29.88	29.88	29.88	
Stack Area	A	ft ²	36.7	36.7	36.7	
Nozzle Diameter (in.)	Dn	in.	0.275	0.275	0.275	
Total Sampling Time	Ø	min.	60	60	60	
Calibration Factor	Y	-	1	1	1	
Pitot Coefficient	Cp	-	0.84	0.84	0.84	
Average Square Root of Velocity Head	√ΔPavg	in. H ₂ O	0.753	0.76	0.749	
Average Orifice Pressure Drop	ΔH	in. H ₂ O	2.01	2.04	2	
Average Meter Temperature	Tm	°F	84	80	78	
Average Stack Pressure	Pg	in. H ₂ O	0.57	0.56	0.57	
Average Stack Temperature	Ts	°F	258	257	256	
Meter Volume @ Meter Conditions	Vm	ft ³	42.16	43.41	43.28	
Total Water Collected	Vlc	ml	261	267	274	
CO ₂ in Stack Gas	CO ₂	%	3.7	5.9	4.5	
O ₂ in Stack Gas	O ₂	%	16.5	16.1	15.9	
CO in Stack Gas	CO	%	0	0	0	
Total Particulate Catch (PM & CPM)	PMt	mg	94.6	24.0	22.8	23.4

CALCULATED VALUES						
Meter Volume	Vmstd	dscf	41.1	42.6	42.6	42.6
Water Vapor in Stack Gas	Bws	%	23.03	22.78	23.23	23.0
Molecular Weight of Stack Gas (dry)	Md	g/g-mole	29.3	29.6	29.4	29.5
Molecular Weight of Stack Gas (wet)	Ms	g/g-mole	26.7	26.9	26.7	26.8
Average Velocity of Stack Gas	Vs	ft/min	3,078	3,088	3,054	3071.0
Actual Stack Gas Flowrate	Q	acf/min	112,963	113,326	112,086	112706.2
Stack Gas Flowrate	Qsd	dscf/min	63,946	64,445	63,461	63952.9
Isokinetics	I	%	95.3	98.1	99.7	98.9

EMISSION CONCENTRATION						
Particulate Emission Concentration	PCgr	gr/acf	2.61E-02	6.40E-03	6.09E-03	6.24E-03
Particulate Emission Concentration	PCgrsd	gr/dscf	3.55E-02	8.69E-03	8.25E-03	8.47E-03
Particulate Emission Concentration	PClbsd	lb/dscf	5.07E-06	1.24E-06	1.18E-06	1.21E-06
Particulate Emission Concentration	PCµgm	µg/dscm	81398	19907	18900	19403.7

EMISSION RATE						
Particulate Emission Rate	PER	lbs/hr	19.47	4.80	4.49	4.64

NOTE: Average includes only Runs 2 and 3.

CAPTURE EFFICIENCY
DATA
LOUISIANA-PACIFIC
9 JULY 1996

	CONCENTRATIONS				FLOW				EMISSION RATES				CAPTURE EFFICIENCY %
	VOC IN SITE 1 ppm	VOC IN SITE 2 ppm	VOC OUT SITE 4 ppm		INLET SITE 1 scfm	INLET SITE 2 scfm	OUTLET SITE 4 scfm		INLET SITE 1 lbs/hr	INLET SITE 2 lbs/hr	INLET 1 & 2 lbs/hr	OUTLET SITE 4 lbs/hr	
Test 1 Average	114.8	184.9	3.3		33,900	33,751	81,266		9.7	15.6	25.3	0.7	97.4
Test 2 Average	94.9	152.9	7.2		39,100	34,488	82,031		9.2	13.1	22.4	1.5	93.4
Test 3 Average	107.0	192.1	3.4		40,844	34,464	80,984		10.9	16.5	27.4	0.7	97.5

TEST PROGRAM AVERAGE	96.1
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EML
CEM SHEET

SOURCE: Louisiana-Pacific Corp.	TEST: 1
DATE: 7/9/96	COLLECTED
METHOD: 3A, 7E, 10, & 25A	BY: ED
UNIT: Thermal Oxidizer Inlet Site 1	WITNESSED
FUEL: Propane	BY: N/A
LOAD: N/A	

STEP	DESCRIPTION	LIMIT	THC	NOx	CO	O2	CO2
1	RANGE		1000	250	1000	25.0	25.0
2	CAL GAS						
	ZERO		0	0	0	0	0
	LOW		283				
	MID	(bias cal. gas)	513	99	498	12.80	12.60
	SPAN		901	241	883	22.6	19.7
3	INT. LOCAL CAL		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		1.8	0.2	3.3	0.1	-0.1
	% ERROR	±2 (±5% for THC)	0.2%	0.1%	0.3%	0.4%	-0.4%
	LOW (PPM OR %)		284.0				
	% ERROR	±2 (±5% for THC)	0.1%				
	MID (PPM OR %)		512.5	97.5	512.5	13.0	12.7
	% ERROR	±2 (±5% for THC)	-0.1%	-0.6%	1.5%	0.8%	0.4%
	HIGH (PPM OR %)		908.9	242.7	882.9	22.5	19.6
	% ERROR	±2 (±5% for THC)	0.8%	0.7%	0.0%	-0.4%	-0.4%
4	INT. BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO		1.8	0.6	2.8	0.1	0.0
	CAL BIAS	±5%	0.0%	0.2%	-0.1%	0.0%	0.4%
	UPSCALE		284.0	97.0	512.3	12.8	12.6
	CAL BIAS	±5%	0.0%	-0.2%	0.0%	-0.8%	-0.4%
5	RESP. TIME (SEC)		30.0	30.0	15.0	15.0	10.0
6	FINAL BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		9.6	1.0	4.0	0.1	0.0
	DRIFT	±3%	0.8%	0.2%	0.1%	0.0%	0.0%
	CAL BIAS	±5%	0.8%	0.3%	0.1%	0.0%	0.4%
	UPSCALE (MID) (PPM OR %)		283.8	100.0	510.0	12.8	12.5
	DRIFT	±3%	0.0%	1.2%	-0.2%	0.0%	-0.4%
	CAL BIAS	±5%	0.0%	1.0%	-0.3%	-0.8%	-0.8%
7	AVG SYSTEM BIAS		THC	NOx	CO	O2	CO2
	ZERO		5.7	0.8	3.4	0.1	0.0
	UPSCALE		283.9	98.5	511.2	12.8	12.6

Test 1	Integrated Avg	THC	NOx	CO	O2	CO2
1515-1615						
	5	99.4	22.1	171.0	16.9	3.9
	10	91.7	23.9	168.5	17.0	3.8
	15	98.6	21.9	202.5	16.8	3.9
	20	105.7	21.1	212.4	16.8	3.9
	25	98.6	22.5	176.2	16.9	3.9
	30	121.3	19.7	247.0	16.6	4.2
	35	122.8				
	40	128.0				
	45	114.0				
	50	137.4				
	55	130.0				
	60	122.0				

RESULTS	THC (ppmwv as CH4)	NOx (ppmdv)	CO (ppmdv)	O2 (%)	CO2 (%)
TEST AVERAGE	114.1	21.9	196.3	16.8	3.9
BIAS CORRECTED	114.8	21.3	189.2	16.9	3.9
FLOWRATE (dscfm)	26,114				
FLOWRATE (scfm)	33900				
lbs/hr	9.70	4.00	21.55		

EMI
CEM SHEET

SOURCE: Louisiana-Pacific Corp.	TEST: 2
DATE: 7/9/96	COLLECTED
METHOD: 3A, 7E, 10, & 25A	BY: ED
UNIT: Thermal Oxidizer Inlet Site 1	WITNESSED
FUEL: Propane	BY: N/A
LOAD: N/A	

STEP	DESCRIPTION	LIMIT	THC	NOx	CO	O2	CO2
1	RANGE		1000	250	1000	25.0	25.0
2	CAL GAS						
	ZERO		0	0	0	0	0
	LOW		283				
	MID	(bias cal. gas)	513	99	498	12.80	12.60
	SPAN		901	241	883	22.6	19.7
3	INT. LOCAL CAL		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		1.8	0.2	3.3	0.1	-0.1
	% ERROR	±2 (±5% for THC)	0.2%	0.1%	0.3%	0.4%	-0.4%
	LOW (PPM OR %)		284.0				
	% ERROR	±2 (±5% for THC)	0.1%				
	MID (PPM OR %)		512.5	97.5	512.5	13.0	12.7
	% ERROR	±2 (±5% for THC)	-0.1%	-0.6%	1.5%	0.8%	0.4%
	HIGH (PPM OR %)		908.9	242.7	882.9	22.5	19.6
	% ERROR	±2 (±5% for THC)	0.8%	0.7%	0.0%	-0.4%	-0.4%
4	INT. BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO		9.6	1.0	4.0	0.1	0.0
	CAL BIAS	±5%	0.8%	0.3%	0.1%	0.0%	0.4%
	UPSCALE		283.8	100.0	510.0	12.8	12.5
	CAL BIAS	±5%	0.0%	1.0%	-0.3%	-0.8%	-0.8%
5	RESP. TIME (SEC)		30.0	30.0	15.0	15.0	10.0
6	FINAL BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		11.3	0.4	2.3	0.2	0.1
	DRIFT	±3%	0.2%	-0.2%	-0.2%	0.4%	0.4%
	CAL BIAS	±5%	1.0%	0.1%	-0.1%	0.4%	0.8%
	UPSCALE (MID) (PPM OR %)		285.6	99.2	509.8	12.8	12.6
	DRIFT	±3%	0.2%	-0.3%	0.0%	0.0%	0.4%
	CAL BIAS	±5%	0.2%	0.7%	-0.3%	-0.8%	-0.4%
7	AVG SYSTEM BIAS		THC	NOx	CO	O2	CO2
	ZERO		10.5	0.7	3.2	0.2	0.1
	UPSCALE		284.7	99.6	509.9	12.8	12.6

Test 2	Integrated Avg	THC	NOx	CO	O2	CO2
1730-1905						
	5	110.5	25.4	206.3	16.7	4.0
	10	110.0	25.5	218.1	16.7	4.1
	15	61.6	24.1	104.4	17.4	3.3
	20	68.7	23.9	135.2	17.3	3.4
	25	78.7	23.0	157.8	17.1	3.5
	30	81.8				
	35	98.6				
	40	96.0				
	45	107.3				
	50	110.1				
	55	105.2				
	60	117.7				

RESULTS	THC	NOx	CO	O2	CO2
	(ppmwv as CH4)	(ppmdv)	(ppmdv)	(%)	(%)
TEST AVERAGE	95.5	24.4	164.4	17.0	3.7
BIAS CORRECTED	94.9	23.7	158.4	17.1	3.6
FLOWRATE (dscfm)	30,687				
FLOWRATE (scfm)	39,100				
lbs/hr	9.25	5.21	21.21		

EML
CEM SHEET

SOURCE: Louisiana-Pacific Corp.	TEST: 3
DATE: 7/9/96	COLLECTED
METHOD: 3A, 7E, 10, & 25A	BY: ED
UNIT: Thermal Oxidizer Inlet Site 1	WITNESSED
FUEL: Propane	BY: N/A
LOAD: N/A	

STEP	DESCRIPTION	LIMIT	THC	NOx	CO	O2	CO2
1	RANGE		1000	250	1000	25.0	25.0
2	CAL GAS						
	ZERO		0	0	0	0	0
	LOW		283				
	MID	(bias cal. gas)	513	99	498	12.80	12.60
	SPAN		901	241	883	22.6	19.7
3	INT. LOCAL CAL		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		1.8	0.2	3.3	0.1	-0.1
	% ERROR	±2 (±5% for THC)	0.2%	0.1%	0.3%	0.4%	-0.4%
	LOW (PPM OR %)		284.0				
	% ERROR	±2 (±5% for THC)	0.1%				
	MID (PPM OR %)		512.5	97.5	512.5	13.0	12.7
	% ERROR	±2 (±5% for THC)	-0.1%	-0.6%	1.5%	0.8%	0.4%
	HIGH (PPM OR %)		908.9	242.7	882.9	22.5	19.6
	% ERROR	±2 (±5% for THC)	0.8%	0.7%	0.0%	-0.4%	-0.4%
4	INT. BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO		11.3	0.4	2.3	0.2	0.1
	CAL BIAS	±5%	1.0%	0.1%	-0.1%	0.4%	0.8%
	UPSCALE		285.6	99.2	509.8	12.8	12.6
	CAL BIAS	±5%	0.2%	0.7%	-0.3%	-0.8%	-0.4%
5	RESP. TIME (SEC)		30.0	30.0	15.0	15.0	10.0
6	FINAL BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		8.7	0.9	1.9	0.1	0.0
	DRIFT	±3%	-0.3%	0.2%	0.0%	-0.4%	-0.4%
	CAL BIAS	±5%	0.7%	0.3%	-0.1%	0.0%	0.4%
	UPSCALE (MID) (PPM OR %)		285.5	100.5	513.0	12.8	12.7
	DRIFT	±3%	0.0%	0.5%	0.3%	0.0%	0.4%
	CAL BIAS	±5%	0.2%	1.2%	0.1%	-0.8%	0.0%
7	AVG SYSTEM BIAS		THC	NOx	CO	O2	CO2
	ZERO		10.0	0.7	2.1	0.2	0.1
	UPSCALE		285.6	99.9	511.4	12.8	12.7
Test 3	Integrated Avg		THC	NOx	CO	O2	CO2
1955-2055							
	5		99.7	18.9	168.9	17.2	3.5
	10		86.7	19.2	180.5	17.1	3.6
	15		88.3	21.1	141.7	17.4	3.4
	20		103.1	20.1	189.9	17.1	3.7
	25		101.3	19.7	194.1	17.0	3.8
	30		111.8				
	35		110.3				
	40		121.4				
	45		112.4				
	50		121.5				
	55		134.4				
	60		103.1				

RESULTS	THC	NOx	CO	O2	CO2
	(ppmwv as CH4)	(ppmdv)	(ppmdv)	(%)	(%)
TEST AVERAGE	107.8	19.8	175.0	17.2	3.6
BIAS CORRECTED	107.0	19.1	169.1	17.2	3.6
FLOWRATE (dscfm)	32,465				
FLOWRATE (scfm)	40,844				
lbs/hr	10.89	4.45	23.95		

EML
CEM SHEET

SOURCE: Louisiana-Pacific Corp.	TEST: 1
DATE: 7/9/96	COLLECTED
METHOD: 3A, 7E, 10, & 25A	BY: ED
UNIT: Thermal Oxidizer Inlet Site 2	WITNESSED
FUEL: Propane	BY: N/A
LOAD: N/A	

STEP	DESCRIPTION	LIMIT	THC	NOx	CO	O2	CO2
1	RANGE		1000	250	1000	25.0	25.0
2	CAL GAS						
	ZERO		0	0	0	0	0
	LOW		283				
	MID	(bias cal. gas)	513	99	498	12.80	12.60
	SPAN		901	241	883	22.6	19.7
3	INT. LOCAL CAL		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		6.2	0.2	3.3	0.1	-0.1
	% ERROR	±2 (±5% for THC)	0.6%	0.1%	0.3%	0.4%	-0.4%
	LOW (PPM OR %)		291.0				
	% ERROR	±2 (±5% for THC)	0.8%				
	MID (PPM OR %)		523.3	97.5	512.5	13.0	12.7
	% ERROR	±2 (±5% for THC)	1.0%	-0.6%	1.5%	0.8%	0.4%
	HIGH (PPM OR %)		906.9	242.7	882.9	22.5	19.6
	% ERROR	±2 (±5% for THC)	0.6%	0.7%	0.0%	-0.4%	-0.4%
4	INT. BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO		6.2	1.3	3.1	0.1	0.1
	CAL BIAS	±5%	0.0%	0.4%	0.0%	0.0%	0.8%
	UPSCALE		291.0	97.6	512.3	12.7	12.5
	CAL BIAS	±5%	0.0%	0.0%	0.0%	-1.2%	-0.8%
5	RESP. TIME (SEC)		30.0	30.0	15.0	15.0	10.0
6	FINAL BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		8.6	1.0	3.7	0.1	0.0
	DRIFT	±3%	0.2%	-0.1%	0.1%	0.0%	-0.4%
	CAL BIAS	±5%	0.2%	0.3%	0.0%	0.0%	0.4%
	UPSCALE (MID) (PPM OR %)		289.0	100.8	510.6	12.8	12.6
	DRIFT	±3%	-0.2%	1.3%	-0.2%	0.4%	0.4%
	CAL BIAS	±5%	-0.2%	1.3%	-0.2%	-0.8%	-0.4%
7	AVG SYSTEM BIAS		THC	NOx	CO	O2	CO2
	ZERO		7.4	1.2	3.4	0.1	0.1
	UPSCALE		290.0	99.2	511.5	12.8	12.6

Test 1	Integrated Avg	THC	NOx	CO	O2	CO2
1515-1615						
	5	149.3				
	10	145.7				
	15	194.6				
	20	174.3				
	25	209.2				
	30	209.7				
	35	196.6	15.8	1046.3	17.2	3.5
	40	215.4	17.8	389.2	17.2	3.5
	45	193.8	17.7	490.5	17.1	3.6
	50	178.3	16.5	418.0	17.2	3.4
	55	171.6	15.5	380.2	17.3	3.3
	60	173.4	16.3	363.1	17.4	3.3

RESULTS	THC (ppmwv as CH4)	NOx (ppmdv)	CO (ppmdv)	O2 (%)	CO2 (%)
TEST AVERAGE	184.3	16.6	514.6	17.2	3.4
BIAS CORRECTED	184.9	15.6	501.0	17.3	3.4
FLOWRATE (dscfm)	25,865				
FLOWRATE (scfm)	33,751				
lbs/hr	15.56	2.89	56.54		

EML
CEM SHEET

SOURCE: Louisiana-Pacific Corp.	TEST: 2
DATE: 7/9/96	COLLECTED
METHOD: 3A, 7E, 10, & 25A	BY: ED
UNIT: Thermal Oxidizer Inlet Site 2	WITNESSED
FUEL: Propane	BY: N/A
LOAD: N/A	

STEP	DESCRIPTION	LIMIT	THC	NOx	CO	O2	CO2
1	RANGE		1000	250	1000	25.0	25.0
2	CAL GAS						
	ZERO		0	0	0	0	0
	LOW		283				
	MID	(bias cal. gas)	513	99	498	12.80	12.60
	SPAN		901	241	883	22.6	19.7
3	INT. LOCAL CAL		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		6.2	0.2	3.3	0.1	-0.1
	% ERROR	±2 (±5% for THC)	0.6%	0.1%	0.3%	0.4%	-0.4%
	LOW (PPM OR %)		291.0				
	% ERROR	±2 (±5% for THC)	0.8%				
	MID (PPM OR %)		523.3	97.5	512.5	13.0	12.7
	% ERROR	±2 (±5% for THC)	1.0%	-0.6%	1.5%	0.8%	0.4%
	HIGH (PPM OR %)		906.9	242.7	882.9	22.5	19.6
	% ERROR	±2 (±5% for THC)	0.6%	0.7%	0.0%	-0.4%	-0.4%
4	INT. BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO		8.6	1.0	3.7	0.1	0.0
	CAL BIAS	±5%	0.2%	0.3%	0.0%	0.0%	0.4%
	UPSCALE		289.0	100.8	510.6	12.8	12.6
	CAL BIAS	±5%	-0.2%	1.3%	-0.2%	-0.8%	-0.4%
5	RESP. TIME (SEC)		30.0	30.0	15.0	15.0	10.0
6	FINAL BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		3.1	1.0	1.6	0.1	-0.1
	DRIFT	±3%	-0.6%	0.0%	-0.2%	0.0%	-0.4%
	CAL BIAS	±5%	-0.3%	0.3%	-0.2%	0.0%	0.0%
	UPSCALE (MID) (PPM OR %)		285.0	100.4	507.8	12.8	12.5
	DRIFT	±3%	-0.4%	-0.2%	-0.3%	0.0%	-0.4%
	CAL BIAS	±5%	-0.6%	1.2%	-0.5%	-0.8%	-0.8%
7	AVG SYSTEM BIAS		THC	NOx	CO	O2	CO2
	ZERO		5.9	1.0	2.7	0.1	-0.1
	UPSCALE		287.0	100.6	509.2	12.8	12.6

Test 2	Integrated Avg	THC	NOx	CO	O2	CO2
1730-1900						
1735	5	117.1				
1740	10	125.4				
1745	15	168.9				
1820	20	184.4				
	25	157.6				
	30	147.1	15.6	208.9	17.7	3.0
	35	180.3	16.3	416.3	17.2	3.5
	40	180.3	16.7	421.8	17.2	3.5
	45	153.9	15.9	342.7	17.4	3.3
	50	161.5	15.8	373.7	17.3	3.4
	55	138.3	15.9	312.6	17.5	3.2
1900	60	143.5	15.9	329.3	17.4	3.2

RESULTS	THC (ppmwv as CH4)	NOx (ppmdv)	CO (ppmdv)	O2 (%)	CO2 (%)
TEST AVERAGE	154.9	16.0	343.6	17.4	3.3
BIAS CORRECTED	152.9	14.9	335.2	17.4	3.4
FLOWRATE (dscfm)	25,862				
FLOWRATE (scfm)	34,488				
lbs/hr	13.15	2.77	37.82		

EML
CEM SHEET

SOURCE: Louisiana-Pacific Corp.	TEST: 3
DATE: 7/9/96	COLLECTED
METHOD: 3A, 7E, 10, & 25A	BY: ED
UNIT: Thermal Oxidizer Inlet Site 2	WITNESSED
FUEL: Propane	BY: N/A
LOAD: N/A	

STEP	DESCRIPTION	LIMIT	THC	NOx	CO	O2	CO2
1	RANGE		1000	250	1000	25.0	25.0
2	CAL GAS						
	ZERO		0	0	0	0	0
	LOW		283				
	MID	(bias cal. gas)	513	99	498	12.80	12.60
	SPAN		901	241	883	22.6	19.7
3	INT. LOCAL CAL		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		6.2	0.2	3.3	0.1	-0.1
	% ERROR	±2 (±5% for THC)	0.6%	0.1%	0.3%	0.4%	-0.4%
	LOW (PPM OR %)		291.0				
	% ERROR	±2 (±5% for THC)	0.8%				
	MID (PPM OR %)		523.3	97.5	512.5	13.0	12.7
	% ERROR	±2 (±5% for THC)	1.0%	-0.6%	1.5%	0.8%	0.4%
	HIGH (PPM OR %)		906.9	242.7	882.9	22.5	19.6
	% ERROR	±2 (±5% for THC)	0.6%	0.7%	0.0%	-0.4%	-0.4%
4	INT. BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO		3.1	1.0	1.6	0.1	-0.1
	CAL BIAS	±5%	-0.3%	0.3%	-0.2%	0.0%	0.0%
	UPSCALE		285.0	100.4	507.8	12.8	12.5
	CAL BIAS	±5%	-0.6%	1.2%	-0.5%	-0.8%	-0.8%
5	RESP. TIME (SEC)		30.0	30.0	15.0	15.0	10.0
6	FINAL BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		3.1	1.0	1.6	0.1	-0.1
	DRIFT	±3%	0.0%	0.0%	0.0%	0.0%	0.0%
	CAL BIAS	±5%	-0.3%	0.3%	-0.2%	0.0%	0.0%
	UPSCALE (MID) (PPM OR %)		285.0	100.4	507.8	12.8	12.5
	DRIFT	±3%	0.0%	0.0%	0.0%	0.0%	0.0%
	CAL BIAS	±5%	-0.6%	1.2%	-0.5%	-0.8%	-0.8%
7	AVG SYSTEM BIAS		THC	NOx	CO	O2	CO2
	ZERO		3.1	1.0	1.6	0.1	-0.1
	UPSCALE		285.0	100.4	507.8	12.8	12.5
Test 3 Integrated Avg			THC	NOx	CO	O2	CO2
1955-2055							
	5		176.9				
	10		191.8				
	15		214.8				
	20		191.4				
	25		178.8				
	30		180.9				
	35		189.5	16.4	216.9	17.7	3.1
	40		194.4	15.2	411.5	17.3	3.4
	45		180.1	15.2	376.0	17.4	3.3
	50		199.7	15.4	483.4	17.3	3.4
	55		213.1	15.6	520.8	17.1	3.6
	60		214.6	15.9	516.0	17.0	3.7

RESULTS	THC (ppmwv as CH4)	NOx (ppmdv)	CO (ppmdv)	O2 (%)	CO2 (%)
TEST AVERAGE	193.8	15.6	420.8	17.3	3.4
BIAS CORRECTED	192.1	14.6	412.4	17.3	3.5
FLOWRATE (dscfm)	25,314				
FLOWRATE (scfm)	34,464				
lbs/hr	16.50	2.64	45.54		

EML
CEM SHEET

SOURCE: Louisiana-Pacific Corp.	TEST: 1
DATE: 7/9/96	COLLECTED
METHOD: 3A, 7E, 10, & 25A	BY: BH
UNIT: Site #4	WITNESSED
FUEL: Propane	BY: N/A
LOAD: N/A	

STEP	DESCRIPTION	LIMIT	THC	NOx	CO	O2	CO2
1	RANGE		100	250	1000	25.0	25.0
2	CAL GAS						
	ZERO		0	0	0	0	0
	LOW		16				
	MID	(bias cal. gas)	49	120	498	12.40	12.30
	SPAN		101	237	884	22.1	19.9
3	INT. LOCAL CAL		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		0.0	0.0	-1.1	0.3	0.3
	% ERROR	±2 (±5% for THC)	0.0%	0.0%	-0.1%	1.2%	1.2%
	LOW (PPM OR %)		14.7				
	% ERROR	±2 (±5% for THC)	-1.6%				
	MID (PPM OR %)		51.3	124.6	514.8	12.7	12.7
	% ERROR	±2 (±5% for THC)	2.4%	1.8%	1.7%	1.2%	1.6%
	HIGH (PPM OR %)		97.0	240.6	872.1	22.0	19.9
	% ERROR	±2 (±5% for THC)	-4.0%	1.4%	-1.2%	-0.4%	0.0%
4	INT. BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO		0.0	-0.8	-0.6	0.3	0.3
	CAL BIAS	±5%	0.0%	-0.3%	0.1%	0.0%	0.0%
	UPSCALE		14.7	123.3	492.0	12.7	12.7
	CAL BIAS	±5%	0.0%	-0.5%	-2.3%	0.0%	0.0%
5	RESP. TIME (SEC)		30.0	30.0	30.0	15.0	20.0
6	FINAL BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		0.0	0.4	16.3	0.1	0.3
	DRIFT	±3%	0.0%	0.5%	1.7%	-0.8%	0.0%
	CAL BIAS	±5%	0.0%	0.2%	1.7%	-0.8%	0.0%
	UPSCALE (MID) (PPM OR %)		17.6	116.2	470.6	12.5	12.0
	DRIFT	±3%	2.9%	-2.8%	-2.1%	-0.8%	-2.8%
	CAL BIAS	±5%	2.9%	-3.4%	-4.4%	-0.8%	-2.8%
7	AVG SYSTEM BIAS		THC	NOx	CO	O2	CO2
	ZERO		0.0	-0.2	7.9	0.2	0.3
	UPSCALE		16.2	119.8	481.3	12.6	12.4

Test 1	Integrated Avg	THC	NOx	CO	O2	CO2
1515-1615						
	5	1.0	16.8	51.7	16.7	3.8
	10	0.4	16.7	46.1	16.6	4.0
	15	0.5	16.6	54.3	16.6	3.9
	20	0.5	16.0	63.7	16.8	3.8
	25	0.8	17.3	60.6	16.7	3.8
	30	0.9	15.8	72.3	16.6	4.0
	35	1.1				
	40	3.4				
	45	3.3				
	50	4.4				
	55	5.1				
	60	15.2				

RESULTS	THC (ppmwv as CH4)	NOx (ppmdv)	CO (ppmdv)	O2 (%)	CO2 (%)
TEST AVERAGE	3.1	16.5	58.1	16.7	3.9
BIAS CORRECTED	3.3	16.7	52.9	16.5	3.7
FLOWRATE (dscfm)	62553				
FLOWRATE (scfm)	81266				
lbs/hr	0.66	7.50	14.43		

EML
CEM SHEET

SOURCE: Louisiana-Pacific Corp.	TEST: 2
DATE: 7/9/96	COLLECTED
METHOD: 3A, 7E, 10, & 25A	BY: BH
UNIT: Site #4	WITNESSED
FUEL: Propane	BY: N/A
LOAD: N/A	

STEP	DESCRIPTION	LIMIT	THC	NOx	CO	O2	CO2
1	RANGE		100	250	1000	25.0	25.0
2	CAL GAS						
	ZERO		0	0	0	0	0
	LOW		16				
	MID	(bias cal. gas)	49	120	498	12.40	12.30
	SPAN		101	237	884	22.1	19.9
3	INT. LOCAL CAL		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		0.0	0.0	-1.1	0.3	0.3
	% ERROR	±2 (±5% for THC)	0.0%	0.0%	-0.1%	1.2%	1.2%
	LOW (PPM OR %)		14.7				
	% ERROR	±2 (±5% for THC)	-1.6%				
	MID (PPM OR %)		51.3	124.6	514.8	12.7	12.7
	% ERROR	±2 (±5% for THC)	2.4%	1.8%	1.7%	1.2%	1.6%
	HIGH (PPM OR %)		97.0	240.6	872.1	22.0	19.9
	% ERROR	±2 (±5% for THC)	-4.0%	1.4%	-1.2%	-0.4%	0.0%
4	INT. BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO		0.0	-0.8	-0.6	0.3	0.3
	CAL BIAS	±5%	0.0%	-0.3%	0.1%	0.0%	0.0%
	UPSCALE		17.6	116.2	470.6	12.5	12.0
	CAL BIAS	±5%	2.9%	-3.4%	-4.4%	-0.8%	-2.8%
5	RESP. TIME (SEC)		30.0	30.0	30.0	15.0	20.0
6	FINAL BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		0.0	0.3	2.7	0.2	0.2
	DRIFT	±3%	0.0%	0.4%	0.3%	-0.4%	-0.4%
	CAL BIAS	±5%	0.0%	0.1%	0.4%	-0.4%	-0.4%
	UPSCALE (MID) (PPM OR %)		17.0	116.7	485.8	12.7	11.4
	DRIFT	±3%	-0.6%	0.2%	1.5%	0.8%	-2.4%
	CAL BIAS	±5%	2.3%	-3.2%	-2.9%	0.0%	-5.2%
7	AVG SYSTEM BIAS		THC	NOx	CO	O2	CO2
	ZERO		0.0	-0.3	1.1	0.3	0.3
	UPSCALE		17.3	116.5	478.2	12.6	11.7

Test 2	Integrated Avg	THC	NOx	CO	O2	CO2
1730-1910						
	5	6.2				
	10	7.5				
	15	7.3				
	20	16.9				
	25	18.2				
	30	14.7				
	35	5.6	6.7	31.7	17.1	3.3
	40	0.9	18.2	57.1	16.3	5.9
	45	1.1	17.5	55.1	16.0	6.0
	50	0.8	17.1	59.0	16.0	6.5
	55	1.0	18.0	60.7	16.2	6.5
	60	1.0	15.1	44.4	16.1	6.2

RESULTS	THC (ppmwv as CH4)	NOx (ppmdv)	CO (ppmdv)	O2 (%)	CO2 (%)
TEST AVERAGE	6.8	15.4	51.3	16.3	5.7
BIAS CORRECTED	7.2	16.1	52.5	16.1	5.9
FLOWRATE (dscfm)	63344				
FLOWRATE (scfm)	82031				
lbs/hr	1.48	7.32	14.50		

EML
CEM SHEET

SOURCE:	Louisiana-Pacific Corp.	TEST:	3
DATE:	7/9/96	COLLECTED	
METHOD:	3A, 7E, 10, & 25A	BY:	BH
UNIT:	Site #4	WITNESSED	
FUEL:	Propane	BY:	N/A
LOAD:	N/A		

STEP	DESCRIPTION	LIMIT	THC	NOx	CO	O2	CO2
1	RANGE		100	250	1000	25.0	25.0
2	CAL GAS						
	ZERO		0	0	0	0	0
	LOW		16				
	MID	(bias cal. gas)	49	120	498	12.40	12.30
	SPAN		101	237	884	22.1	19.9
3	INT. LOCAL CAL		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		0.0	0.0	-1.1	0.3	0.3
	% ERROR	±2 (±5% for THC)	0.0%	0.0%	-0.1%	1.2%	1.2%
	LOW (PPM OR %)		14.7				
	% ERROR	±2 (±5% for THC)	-1.6%				
	MID (PPM OR %)		51.3	124.6	514.8	12.7	12.7
	% ERROR	±2 (±5% for THC)	2.4%	1.8%	1.7%	1.2%	1.6%
	HIGH (PPM OR %)		97.0	240.6	872.1	22.0	19.9
	% ERROR	±2 (±5% for THC)	-4.0%	1.4%	-1.2%	-0.4%	0.0%
4	INT. BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO		0.0	-0.8	-0.6	0.3	0.3
	CAL BIAS	±5%	0.0%	-0.3%	0.1%	0.0%	0.0%
	UPSCALE		17.0	116.7	485.8	12.7	11.4
	CAL BIAS	±5%	2.3%	-3.2%	-2.9%	0.0%	-5.2%
5	RESP. TIME (SEC)		30.0	30.0	30.0	15.0	20.0
6	FINAL BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		0.0	3.6	3.5	0.3	0.3
	DRIFT	±3%	0.0%	1.8%	0.4%	0.0%	0.0%
	CAL BIAS	±5%	0.0%	1.4%	0.5%	0.0%	0.0%
	UPSCALE (MID) (PPM OR %)		16.3	118.2	479.0	12.6	12.0
	DRIFT	±3%	-0.7%	0.6%	-0.7%	-0.4%	2.4%
	CAL BIAS	±5%	1.6%	-2.6%	-3.6%	-0.4%	-2.8%
7	AVG SYSTEM BIAS		THC	NOx	CO	O2	CO2
	ZERO		0.0	1.4	1.5	0.3	0.3
	UPSCALE		16.7	117.5	482.4	12.7	11.7

Test 3	Integrated Avg	THC	NOx	CO	O2	CO2
1955-2055						
	5	7.3				
	10	7.0				
	15	7.1				
	20	7.1				
	25	7.0				
	30	8.0				
	35	6.9	NA	NA	NA	NA
	40	1.5	15.7	63.1	16.4	5.0
	45	1.3	16.9	63.9	16.1	4.5
	50	1.6	16.8	69.2	16.1	4.6
	55	1.2	15.9	68.0	16.6	4.2
	60	0.8	16.3	42.2	15.6	4.0

RESULTS	THC (ppmwv as CH4)	NOx (ppmdv)	CO (ppmdv)	O2 (%)	CO2 (%)
TEST AVERAGE	4.7	16.3	61.3	16.2	4.5
BIAS CORRECTED	3.4	15.4	62.0	15.9	4.5
FLOWRATE (dscfm)	62173				
FLOWRATE (scfm)	80984				
lbs/hr	0.70	6.87	16.80		

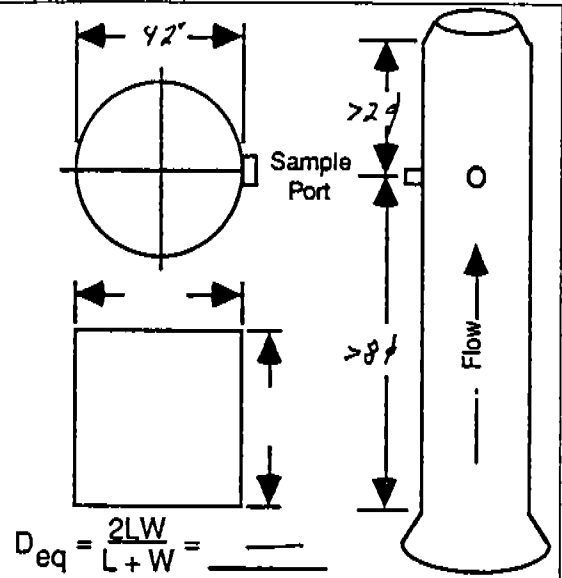
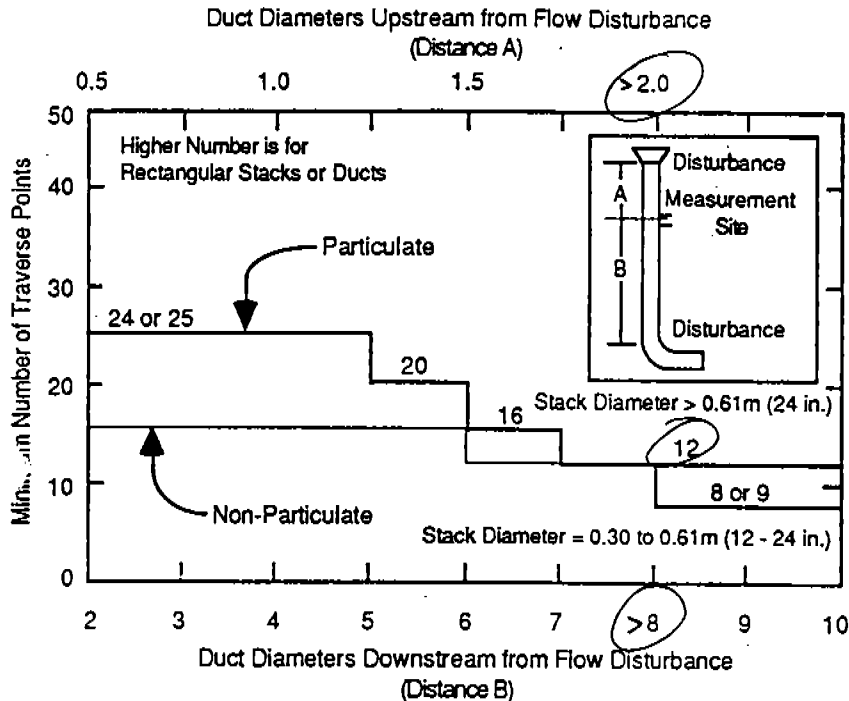
APPENDIX C

Field Data

Firm LOUISIANA PACIFIC CORP
Date 9 JULY 96 Project No. 96053
Location #1
Diameters Upstream > 24
Diameters Downstream 78

Total Traverse Points Required 12
Number of Ports 2
Points Per Port 6
Probe Traverses: Horizontal X
Vertical X

MINIMUM NUMBER OF TRAVERSE POINTS FOR PARTICULATE AND NON-PARTICULATE TRAVERSES



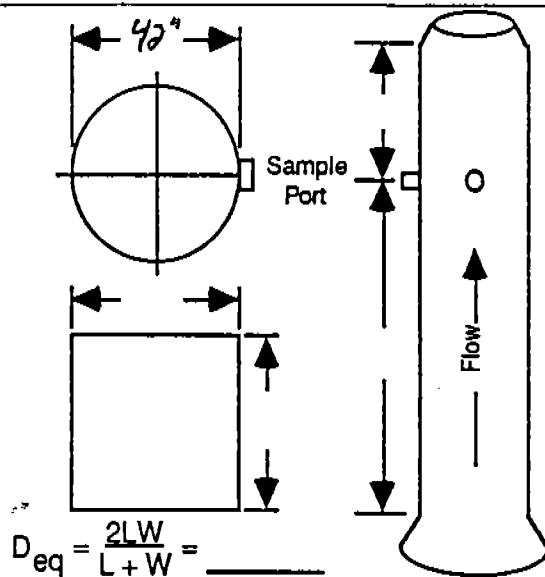
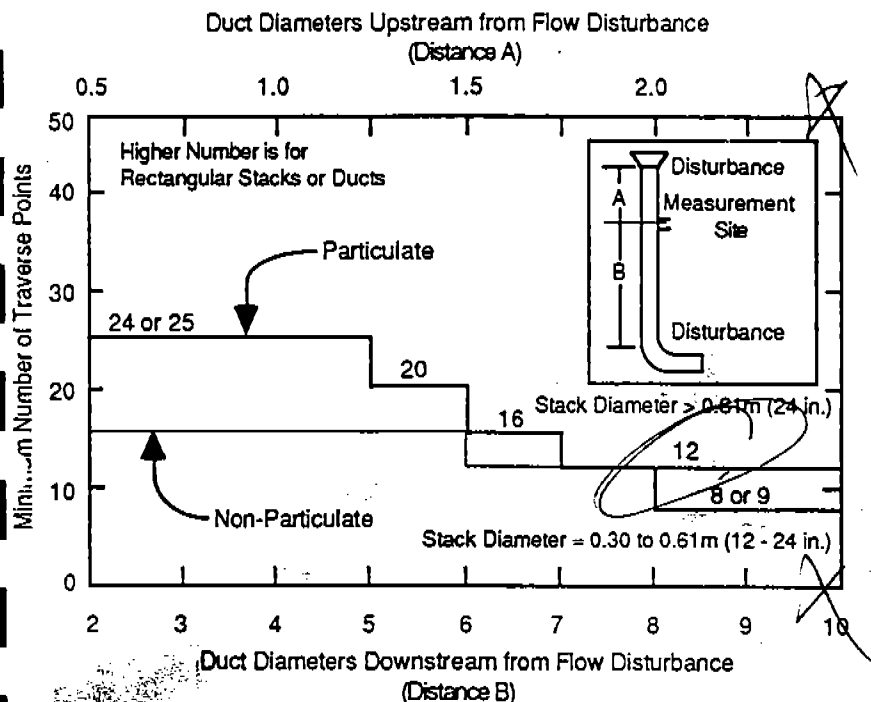
Cross-Sectional Layout For Rectangular Stacks

Traverses	Matrix
9	3x3
12	4x3
16	4x4
20	5x4
25	5x5

Point On A Diameter	Location of Traverse Points in Circular Stacks*					Traverse Point Location		
	Number of Traverse Points on a Diameter					Distance From Wall	Nipple Size	Total Distance
	4	6	8	10	12			
1	6.7	4.4	3.2	2.6	2.1	1.85	6"	7.9
2	25.0	14.6	10.5	8.2	6.7	6.13		12.1
3	75.0	29.6	19.4	14.6	11.8	12.43		18.4
4	93.3	70.4	32.3	22.6	17.7	29.57		35.6
5		85.4	67.7	34.2	25.0	35.87		41.9
6		95.6	80.6	65.8	35.6	40.15		46.2
7			89.5	77.4	64.4			
8			96.8	85.4	75.0			
9				91.8	82.3			
10				97.4	88.2			
11					93.3			
12					97.9			

*Percent of Stack Diameter from Inside Wall to Traverse Point

Firm LOUISIANA - PACIFIC
 Date 7/9/96 Project No. 96053
 Location #2
 Diameters Upstream 3"
 Diameters Downstream 10"

 Total Traverse Points Required 12
 Number of Ports 2
 Points Per Port 6
 Probe Traverses: Horizontal YES 10#3
 Vertical YES 10#2
**MINIMUM NUMBER OF TRAVERSE POINTS FOR PARTICULATE
AND NON-PARTICULATE TRAVERSES**

Cross-Sectional Layout For Rectangular Stacks

Traverses	Matrix
9	3x3
12	4x3
16	4x4
20	5x4
25	5x5

Point On A Diameter	Location of Traverse Points in Circular Stacks*					Traverse Point Location		
	Number of Traverse Points on a Diameter					Distance From Wall	Nipple Size	Total Distance
	4	6	8	10	12			
1	6.7	4.4	3.2	2.6	2.1	1.85	6"	7.9
2	25.0	14.6	10.5	8.2	6.7	6.13		12.1
3	75.0	29.6	19.4	14.6	11.8	12.43		18.4
4	93.3	70.4	32.3	22.6	17.7	29.57		35.6
5		85.4	67.7	34.2	25.0	35.87		41.9
6		95.6	80.6	65.8	35.6	40.15		46.2
7			89.5	77.4	64.4			
8			96.8	85.4	75.0			
9				91.8	82.3			
10				97.4	88.2			
11					93.3			
12					97.9			

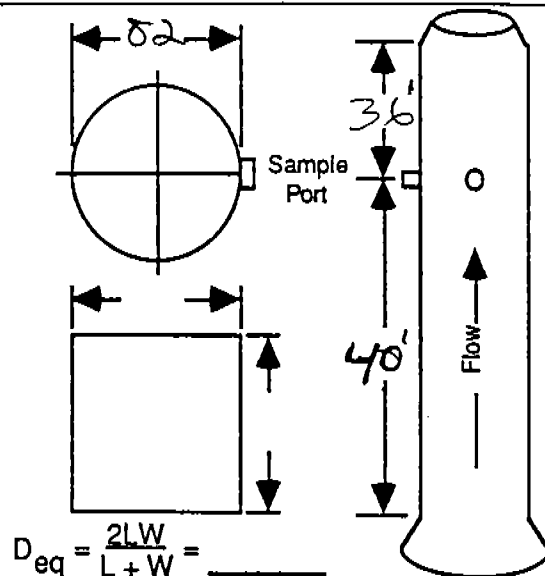
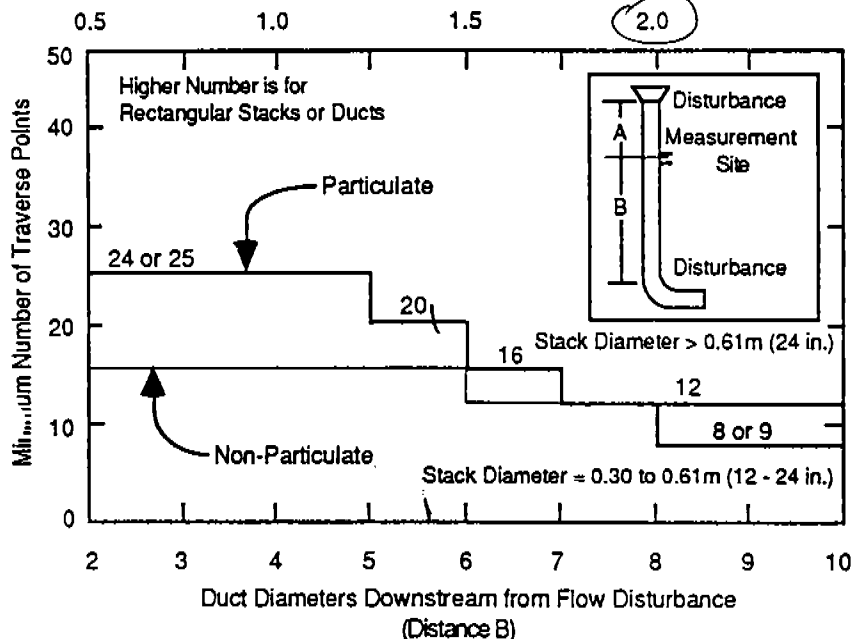
*Percent of Stack Diameter from Inside Wall to Traverse Point

Firm LP
Date 7-9-96 Project No. 96053
Location STACK
Diameters Upstream 5.85
Diameters Downstream 5.27

Total Traverse Points Required 20
Number of Ports 2
Points Per Port 10
Probe Traverses: Horizontal ✓
Vertical

MINIMUM NUMBER OF TRAVERSE POINTS FOR PARTICULATE AND NON-PARTICULATE TRAVERSES

Duct Diameters Upstream from Flow Disturbance
(Distance A)



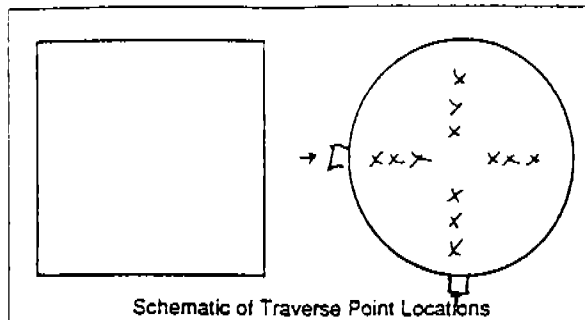
Cross-Sectional Layout For Rectangular Stacks

Traverses	Matrix
9	3x3
12	4x3
16	4x4
20	5x4
25	5x5

Point On A Diameter	Location of Traverse Points in Circular Stacks*					Traverse Point Location		
	Number of Traverse Points on a Diameter					Distance From Wall	Nipple Size	Total Distance
	4	6	8	10	12			
1	6.7	4.4	3.2	2.6	2.1	2.13	6	8.13
2	25.0	14.6	10.5	8.2	6.7	6.7		12.7
3	75.0	29.6	19.4	14.6	11.8	11.9		17.9
4	93.3	70.4	32.3	22.6	17.7	18.5		24.5
5		85.4	67.7	34.2	25.0	28		34
6		95.6	80.6	65.8	35.6	54		60
7			89.5	77.4	64.4	63.5		69.5
8			96.8	85.4	75.0	70		76
9				91.8	82.3	75.3		81.3
10				97.4	88.2	79.8		85.8
11					93.3			
12					97.9			

*Percent of Stack Diameter from Inside Wall to Traverse Point

Firm LOUISIANA PACIFIC CORP
Date 9 JULY 96 Project No. 96053
Location INLET #1
Round Stack or Duct:
Diameter (in) 42" Area 9.62 ft²
Rectangular Stack or Duct:
Stack Length (in) - Area - ft²
Stack Width (in) -
Barometric Pressure; Pb = 29.95 in. Hg
Stack Static Pressure; Pg = -10.2" H₂O in. Hg
Stack Gas Moisture Content; % H₂O = 20%
Stack Gas Molecular Weight; (wet) Mw = 28
Pitot Tube No. 601 Cp = 0.84
Field Tester(s) MM PO
Test Start Time: 0945 Finish: 0950



Cyclonic Flow Angle: + Ø Clockwise
- Ø Counterclockwise

0.221 CALC NOZZLE 0.244 ACTUAL NOZZLE

PORT	POINT	ΔP (Inch H ₂ O)	√ΔP	Ts (°F)	± Ø	Pitots Reversed for Negative Flow?	RADIANS	√ΔP*cosØ
1(V)	1	1.8	1.342	220	0°	-	0	
	2	1.7	1.304	219		-		
	3	1.7	1.304	220		-		
	4	1.7	1.304	219		-		
	5	1.7	1.304	219		-		
	6	1.8	1.342	220		-		
2(H)	1	1.6	1.265	220		-		
	2	1.9	1.378	220		-		
	3	1.8	1.342	219		-		
	4	1.7	1.304	220		-		
	5	1.6	1.265	221		-		
	6	0.99	0.995	207	✓	-	✓	
AVE		1.666						
AVERAGE			1.287	218.7			AVERAGE	

Absolute Gas Temperature; Tst = Ts + 460°

Absolute Gas Pressure; Ps = Pb + Pg/13.6

Gas Velocity; Vs = (85.49)Cp(√ΔP*cosØ)avg/(Ts avg/(Ps*Mw))

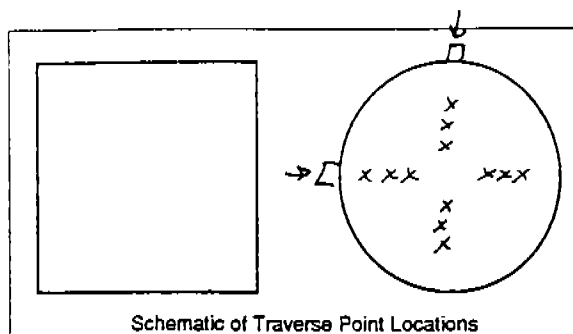
Actual Gas Flow Rate; Qa = (Vs)(60)(A)

Standard Gas Flow Rate; Qsa = Qa(528°R/Tst)(Ps/29.92)

Dry Standard Gas Flow Rate; Qsd = Qsa(528°R/Tst)(Ps/29.92)((100-%H₂O)/100)

678.7°R
29.2 In. Hg
~~34.206~~ ft/sec 8304
48.600 acfm 47928
36.900 scfm 36.573
27.520 dscfm 0.60
29.098 PPM with 0.60
Page 1 of 2

Firm LOUISIANA PACIFIC CORP.
 Date 1 JULY 96 Project No. 96053
 Location INLET #2
 Round Stack or Duct:
 Diameter (in) 42" Area 7.62 ft²
 Rectangular Stack or Duct:
 Stack Length (in) - Area - ft²
 Stack Width (in) -
 Barometric Pressure; Pb = 29.95 in. Hg
 Stack Static Pressure; Pg = -8" H₂O in. Hg
 Stack Gas Moisture Content; % H₂O = 202 (ASSUMED)
 Stack Gas Molecular Weight; (wet) Mw = -
 Pitot Tube No. 401 Cp = 0.84
 Field Tester(s) MM TC PO
 Test Start Time: 0930 Finish: 0939



Cyclonic Flow Angle: + Ø Clockwise
 - Ø Counterwise

PORT	POINT	ΔP (Inch H ₂ O)	√ΔP	Ts (°F)	± Ø	Pitots Reversed for Negative Flow?	RADIANS	√ΔP*cosØ
1 (H)	1	1.2	1.095	251	0°	—	0	
	2	1.5	1.225	252		—		
	3	1.6	1.265	251		—		
	4	1.5	1.225	250		—		
	5	1.4	1.183	248		—		
	6	1.1	1.049	240		—		
2 (V)	1	1.2	1.095	240		—		
	2	1.4	1.183	247		—		
	3	1.5	1.225	250		—		
	4	1.6	1.265	249		—		
	5	1.5	1.225	247		—		
	6	1.1	1.049	243	✓	—	✓	
		1.383						
AVERAGE			1.072	247.3			AVERAGE	

Absolute Gas Temperature; Tst = Ts + 460°

Absolute Gas Pressure; Ps = Pb + Pg/13.6

Gas Velocity; Vs = (85.49)Cp(√ΔP*cosØ)avg√(Tst avg/(Ps*Mw))

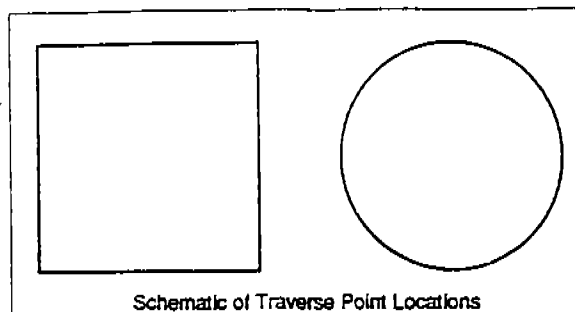
Actual Gas Flow Rate; Qa = (Vs)(60)(A)

Standard Gas Flow Rate; Qs = Qa(528°R/Tst)(Ps/29.92)

 Dry Standard Gas Flow Rate; Qsd = Qa(528°R/Tst)(Ps/29.92)((100-%H₂O)/100)

707.3 °R
29.36 in. Hg
71.40 ft/sec 77.0y
41,214 acfm 44,466
30,130 scfm 32,589
24,150 dscfm 26,071
25,775

Firm LOUISIANA PACIFIC
 Date 9 JULY 96 Project No. 96053
 Location JACK
 Round Stack or Duct:
 Diameter (in) 82" Area ft²
 Rectangular Stack or Duct:
 Stack Length (in) Area ft²
 Stack Width (in)
 Barometric Pressure; Pb = 29.92 in. Hg
 Stack Static Pressure; Pg = -.26 in. H₂O
 Stack Gas Moisture Content; % H₂O = 20 (Assumed)
 Stack Gas Molecular Weight; (wet) Mw = 28 (Assumed)
 Pitot Tube No. 902 Cp = 0.84
 Field Tester(s) MA AK OT
 Test Start Time: 11:45 Finish: 11:30



Cyclonic Flow Angle: + Ø Clockwise
 - Ø Counterwise

CALC NOSE .273 ACTUAL .275

PORT	POINT	ΔP (Inch H ₂ O)	√ΔP	Ts (°F)	± Ø	Pitots Reversed for Negative Flow?	RADIANS	√ΔP*cosØ
	1	.58	0.762	257				
	2	.63	0.794	258				
	3	.63	0.794	260				
	4	.64	0.8	261				
	5	.63	0.794	262				
	6	.58	0.762	254				
	7	.61	0.781	255				
	8	.61	0.781	257				
	9	.59	0.768	259				
	10	.50	0.707	259				
	1	.57	0.755	258				
	2	.57	0.755	255				
	3	.61	0.781	254				
	4	.60	0.775	252				
	5	.61	0.781	253				
	6	.59	0.768	254				
	7	.59	0.768	255				
	8	.58	0.762	257				
	9	.57	0.755	261				
	10	.52	0.721	259				
		.56						
AVERAGE			0.768	257			AVERAGE	

Absolute Gas Temperature; Tst = Ts + 460°

Absolute Gas Pressure; Ps = Pb + Pg/13.6

Gas Velocity; Vs = (85.49)Cp(√ΔP*cosØ)avg√(Tst avg/(Ps*Mw))

Actual Gas Flow Rate; Qa = (Vs)(60)(A)

Standard Gas Flow Rate; Qs = Qa(528°R/Tst)(Ps/29.92)

Dry Standard Gas Flow Rate; Qsd = Qa(528°R/Tst)(Ps/29.92)((100-%H₂O)/100)

66.38

717.1 °R

29.77 in. Hg

50.99 ft/sec

112.193 acfm

82.745 scfm

66.196 dscfm

Client/Firm LP

Location STACK

Project No. 4053 Test Number 1

Testers Initials DT/DK Test Date 7-9-76 Nozzle Size 1.275

Test Time (min) 60 Start Time 1515 Nozzle No.

Mn Per Point 3 End Time 1616 C/K Factor 3.57

Assumed

Moisture 20 (%)

Pb = 29.88 (in Hg)

Probe = 2.03 (in Hg)

Y = 1.00

Probe No. 102

Pilot No. 402

Filter No. 31968

Module No. 98

$\Delta H_0 =$ 2.03

Cp = 0.84

Y = 1.00

Probe No. 102

Pilot No. 402

Filter No. 31968

Signature of Train Operator: Don Koff

Rectangular Stack: Length (in) N/A Width (in) N/A

Circular Stack: Diameter (in) 28.4 Area (ft²) 31.67

Train Leak Checks: Pre-Test 0.0 cfm Post-Test 0.0 cfm

Orsat Leak Check: Pre-Test N/A Post-Test N/A

Pilot Leak Check: Pre-Test ✓ Post-Test ✓

Final Orsat Analysis CO₂ 02%

Port	Point	Time (min)	Meter Volume (ft ³)	ΔP (in. H ₂ O)	ΔH (in. H ₂ O)	Temperatures					Vacuum (in. Hg)	Comments				
						Stack (°F)	Probe (°F)	Hir Box (°F)	Filter (°F)	Cond Oil (°F)			Module Meter			
A			483.00	.52	1.83	255	246	232		42	79	78	4	Static Pressure: In H ₂ O		
	1		485.6	.52	2.01	256	246	231		43	81	78	4			
	2		488.0	.59	2.1	255	247	232		45	84	79	5			
	3		490.0	.60	2.1	253	247	237		48	85	79	5			
	4		492.3	.60	2.1	259	247	237		50	86	80	5			
	5		494.6	.57	2.0	259	247	238		52	86	80	5			
	6		496.9	.57	2.0	256	247	238		53	86	80	5			
	7		499.1	.56	1.99	253	246	237		53	87	81	5			
	8		501.4	.55	1.96	258	246	236		53	86	81	5			
	9		503.6	.53	1.84	260	246	236		53	86	81	5			
B	10		506.2	.75												
	1		508.0	.53	1.89	252	244	235		53	85	81	5			
	2		510.1	.57	2.0	253	244	235		52	85	81	5			
	3		512.2	.59	2.1	253	245	235		52	86	81	5			
	4		514.3	.60	2.1	260	246	231		52	86	81	5			
	5		515.2	.58	2.07	255	246	235		53	86	81	5			
	6		517.1	.58	2.07	262	246	235		52	86	81	5			
	7		519.4	.57	2.0	260	246	235		52	86	81	5			
	8		521.6	.57	2.0	255	245	236		52	86	81	5			
	9		523.2	.57	2.0	262	246	232		53	86	81	5			
	10		524.9	0.57	1.89	259	245	233		53	86	81	5			
													Impinger Recovery			
													Impinger Number	Vol or Wt		Total
														Initial	Final	Catch
													1	100	324	324
													2	100	134	134
													3	0	3	3
													4			
													Other(s)			
													Silica Gel			

Final Reading:

Total Volume:

Average

Avg Square Root ΔP

83.5

Average of In & Out Meter Temperatures

201

Total Moisture Catch:

Calculated Moisture Content:

29.88

EPA Method 5

Particulate Test Data Sheet

Signature of Train Operator:

Client/Firm	LP	Module No.	98	Rectangular Stack: Length (in)	14	Width (in)	N/A
Location	STACK	ΔH@	2.03	Circular Stack: Diameter (in)	02	Area (ft²)	36.67
Project No.	4053	Moisture	20 (%)	Train Leak Checks: Pre-Test	0.0 cfm	In Hg	
Testers Initials	DR/PL	Pb =	29.88 (in Hg)	Post-Test	0.0 cfm	In Hg	
Test Date	7-9-96	Nozzle Size	2.25	Orsat Leak Check: Pre-Test	N/A	Post-Test	N/A
Start Time	1730	Nozzle No.	902	Pilot Leak Check: Pre-Test	✓	Post-Test	✓
End Time	1910	C/K Factor	3.57	Final Orsat Analysis	CEM 02%	CO ₂ %	0.0
Min Per Point	3						

Port	Point	Time (min)	Meter Volume (ft³/g)	ΔP (in. H ₂ O)	ΔH (in. H ₂ O)	Temperatures				Vacuum (in. Hg)	Comments
						Stack (°F)	Probe (°F)	Hir Box (°F)	Filter (°F)	Cond Out (°F)	Module Meter In (°F) Out (°F)
A	1	3	527.300	.56	1.99	250	245	235		47	78
	2	6	529.0	.60	2.14	257	246	238		44	79
	3	9	531.3	.60	2.14	258	247	237		52	81
	4	12	533.8	.62	2.21	254	247	238		56	83
	5	15	536.2	.61	2.18	254	248	237		54	83
	6	18	538.4	.61	2.18	262	247	240		54	83
	7	21	541.1	.57	2.03	260	247	238		45	78
	8	24	543.4	.54	1.93	261	247	240		49	78
	9	27	545.7	.53	1.89	255	246	235		53	79
	10	30	547.9	.48	1.71	252	245	242		54	80
B	1	3	552.1	.52	1.85	257	246	242		55	80
	2	6	554.4	.60	2.14	254	246	241		55	81
	3	9	556.6	.62	2.21	260	247	240		58	82
	4	12	557.1	.63	2.25	259	248	241		61	82
	5	15	561.6	.60	2.14	255	248	241		64	83
	6	18	563.9	.59	2.10	255	248	241		64	84
	7	21	566.2	.58	2.07	263	248	241		54	84
	8	24	568.5	.60	2.14	260	247	240		50	84
	9	27	570.3	.53	1.89	254	247	241		48	84
	10	30	572.810	.46	1.64	257	246	240		48	83
Average						2.04	257				80
Average of In & Out Meter Temperatures											26.7

Impinger Number	Impinger Vol or Wt	Total Catch	
		Initial	Final
1	100	335	235
2	100	130	30
3	0	0	2
4			
Other(s)			
Silica Gel			

Final Reading:	43.41	76
Total Volume:	43.41	76
Avg Square Root ΔP	2.04	257
Calculated Moisture Content:		

Client/Firm LP
 Location STACK
 Project No. 4053 Test Number 3
 Testers Initials DR Test Date 7-9-76
 Test Time (min) 30 Start Time 1950
 Min Per Point 3 End Time 2000 C/K Factor 3.57

Assumed Moisture 20 (%)
 ΔH₂₀ = 2.03
 Cp = 0.84
 Y = 6.00
 Probe No. 902
 Pilot No. 902
 Filter No. 31970

Signature of Train Operator: Dunk
 Rectangular Stack: Length (in) 12 Width (in) 12
 Circular Stack: Diameter (in) 82 Area (ft²) 5.32
 Train Leak Checks: Pre-Test 0.0 cfm Post-Test 0.0 cfm
 Orsat Leak Check: Pre-Test 1/2 Post-Test 1/2
 Pilot Leak Check: Pre-Test 1/2 Post-Test 1/2
 Final Orsat Analysis CO₂ 02%

Port	Point	Time (min)	Meter Volume (ft ³)	ΔP (in. H ₂ O)	ΔH (in. H ₂ O)	Temperatures				Vacuum (in. Hg)	Comments
						Stack (°F)	Probe (°F)	Hot Box (°F)	Filter (°F)	Cond Out (°F)	Module Meter In (°F) Out (°F)
A	1	3	573.000	.55	1.96	253	248	270			75 76
	2	6	575.3	.57	2.03	258	247	274			74 76
	3	9	577.6	.60	2.14	260	248	257			74 75
	4	12	579.7	.63	2.25	255	249	258			75 75
	5	15	582.2	.61	2.17	255	249	260			75 75
	6	18	584.6	.58	2.07	263	249	261			76 74
	7	21	586.7	.57	2.03	258	249	260			77 74
	8	24	589.3	.56	1.99	255	248	260			77 74
	9	27	591.4	.52	1.85	256	248	260			78 74
	10	30	593.7	.46	1.64	261	247	260			78 74
B	1		575.5	.75		252	245	261			77 74
	2		578.0	.52	1.85	252	245	261			77 74
	3		600.5	.57	2.03	253	247	259			78 73
	4		602.5	.59	2.10	260	247	260			79 74
	5		605.2	.58	2.07	254	248	260			80 74
	6		607.3	.54	1.93	254	247	259			80 74
	7		609.8	.57	2.03	263	247	259			80 74
	8		612.0	.58	2.07	261	247	258			80 74
	9		614.3	.58	2.07	261	247	259			80 74
	10		616.4	.55	1.96	254	246	258			79 74
			618.780	.50	1.78	256	246	259			74
Final Reading:						2.00	256	Average			
Total Volume:						43.28	.749	Avg Square Root ΔP			
Average of In & Out Meter Temperatures						78					274

Impinger Recovery			
Impinger Number	Vol or Wt	Initial	Final
1	100	245	245
2	100	129	129
3			
4			
Other(s)			
Silica Gel			

Total Moisture Catch: _____ Calculated Moisture Content: _____

LABORATORY ANALYSIS REPORT

RECEIVED JUL 20 1996
Environmental Health Laboratory
a division of CIGNA Loss Control Services, Inc.
100 Sebethe Drive, Suite A-5
Cromwell, CT 06416
(800) 243-4903
Cromwell (203) 635-6475



Laboratories in Macon, GA and Cromwell, CT

To: Tony Saltis
Air Pollution Characterization & Control
60 Industrial Park Road West
Tolland, CT 06084

Report No.: 96G1087

P. O. No.: 2896

Date Received: 7/12/96

Date Reported: 7/25/96

Analysis: Determination of Condensible Particulate Emissions from Stationary Sources
Analytical Method: EPA Method 202

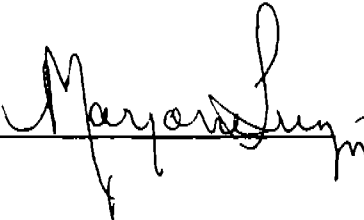
Sample Number	mg Inorganic Condensible Particulate Matter	mg Organic Condensible Particulate Matter	mg Total Condensible Particulate Matter
S1 Run 1	80	48	128
S1 Run 2	59	32	91
S1 Run 3	61	32	93
S3 Run 1	71	34	105
S3 Run 2	19	77	96
S3 Run 3	19	19	38
S4 Run 1	18	74	92
S4 Run 2	11	12	23
S4 Run 3	7.5	15	22

A blank was not provided for the analysis. We recommend that a blank control be submitted with each set of samples so that the sampling media can be checked for possible contamination.

As per the method, all inorganic fractions were checked for the possibility of a positive Ammonium Ion interference. All samples except S4 Run 1 indicated that this interference may exist. Further analysis by ion chromatography would be able to determine the amount of this interference, and samples could be corrected if necessary.

Analyst:


David Torzillo and Marjorie Luzzi


Date: 7/25/96

< = Less than

Lovick

DESCRIPTION

SEND TO:

S3Rn 30I

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1721

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Received by: (Signature)

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✓
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284

APCC CHAIN OF CUSTODY

60 INDUSTRIAL PARK ROAD WEST

TOLLAND CT, 06084

203-871-8557

PROJECT
DESCRIPTION

Lowie P

PROJECT NO. 96053

PROJECT NAME

Lowie P

9661087

FIELD

SAMPLE

NUMBER

DATE

TIME

COMPOSITE
OR GRABANALYSIS
REQUIREDSAMPLING
TRAINSAMPLE
DESCRIPTION

SPECIAL NOTES

SEND TO:

✓ 54 Run 1m

7/9/96

method 202

Meth C1

EHL

✓ 54 Run 10I

.OI H₂O

✓ 54 Run 2m

Meth C1

✓ 54 Run 20I

DI

✓ 54 Run 3m

meth

✓ 54 Run 30I

OI

Relinquished by: (Signature)

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Received by: (Signature)

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*** RESET AVERAGE 07:45:00 26 7.6 PPH
*** RESET AVERAGE 07:45:00 25 7.3 PPH
*** RESET AVERAGE 07:45:00 24 7.1 PPH
*** RESET AVERAGE 07:45:00 23 6.9 PPH
*** RESET AVERAGE 07:45:00 22 6.7 PPH
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$$\begin{array}{c} \text{30.60} \\ \text{71.40} \\ \text{102.00} \\ \text{132.60} \\ \text{163.20} \\ \text{193.80} \\ \text{224.40} \\ \text{255.00} \\ \text{285.60} \\ \text{316.20} \\ \text{346.80} \\ \text{377.40} \\ \text{408.00} \\ \text{438.60} \\ \text{469.20} \\ \text{500.00} \end{array}$$
[illegible]

***** LOS ERP 1 *****		***** UNIV 04 *****		***** STARS FH 07 58:44 *****		***** ENDS FH 07 58:44 *****		***** JUL 08 58 *****	
FT	DATE	UNITS	ST	UNITS	ST	UNITS	ST	UNITS	ST
01	02-1	PC	02-1	PC	03-2	PPH	04	04	04
02	02-1	PC	02-1	PC	03-2	PPH	04	04	04
03	02-1	PC	02-1	PC	03-2	PPH	04	04	04
04	02-1	PC	02-1	PC	03-2	PPH	04	04	04
05	02-1	PC	02-1	PC	03-2	PPH	04	04	04
06	02-1	PC	02-1	PC	03-2	PPH	04	04	04
07	02-1	PC	02-1	PC	03-2	PPH	04	04	04
08	02-1	PC	02-1	PC	03-2	PPH	04	04	04
09	02-1	PC	02-1	PC	03-2	PPH	04	04	04
10	02-1	PC	02-1	PC	03-2	PPH	04	04	04
11	02-1	PC	02-1	PC	03-2	PPH	04	04	04
12	02-1	PC	02-1	PC	03-2	PPH	04	04	04
13	02-1	PC	02-1	PC	03-2	PPH	04	04	04
14	02-1	PC	02-1	PC	03-2	PPH	04	04	04
15	02-1	PC	02-1	PC	03-2	PPH	04	04	04
16	02-1	PC	02-1	PC	03-2	PPH	04	04	04
17	02-1	PC	02-1	PC	03-2	PPH	04	04	04
18	02-1	PC	02-1	PC	03-2	PPH	04	04	04
19	02-1	PC	02-1	PC	03-2	PPH	04	04	04
20	02-1	PC	02-1	PC	03-2	PPH	04	04	04
21	02-1	PC	02-1	PC	03-2	PPH	04	04	04
22	02-1	PC	02-1	PC	03-2	PPH	04	04	04
23	02-1	PC	02-1	PC	03-2	PPH	04	04	04
24	02-1	PC	02-1	PC	03-2	PPH	04	04	04
25	02-1	PC	02-1	PC	03-2	PPH	04	04	04
26	02-1	PC	02-1	PC	03-2	PPH	04	04	04
27	02-1	PC	02-1	PC	03-2	PPH	04	04	04
28	02-1	PC	02-1	PC	03-2	PPH	04	04	04
29	02-1	PC	02-1	PC	03-2	PPH	04	04	04
30	02-1	PC	02-1	PC	03-2	PPH	04	04	04
31	02-1	PC	02-1	PC	03-2	PPH	04	04	04
32	02-1	PC	02-1	PC	03-2	PPH	04	04	04
33	02-1	PC	02-1	PC	03-2	PPH	04	04	04
34	02-1	PC	02-1	PC	03-2	PPH	04	04	04
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36	02-1	PC	02-1	PC	03-2	PPH	04	04	04
37	02-1	PC	02-1	PC	03-2	PPH	04	04	04
38	02-1	PC	02-1	PC	03-2	PPH	04	04	04
39	02-1	PC	02-1	PC	03-2	PPH	04	04	04
40	02-1	PC	02-1	PC	03-2	PPH	04	04	04
41	02-1	PC	02-1	PC	03-2	PPH	04	04	04
42	02-1	PC	02-1	PC	03-2	PPH	04	04	04
43	02-1	PC	02-1	PC	03-2	PPH	04	04	

Handwritten signature: *U. H. P. P.*

[illegible]

11/20/20

[illegible]

```

***** LDE ERP 1 ***** UNIT 01
***** STARTS ET 08 23:54 ***** ENDS AT 08 13:55 *****
*****

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Site 2

*** LD3 GRP 1 *** UNIT 01 *** STARTS AT 14:09:37 *** ENDS AT 14:09:37 *** JUL 09 1994 ***

PT	DATA	UNITS	ST	LEADER	RT	DATA	UNITS	ST	LEADER
01	1	1	1	1	01	1	1	1	1
02	1	1	1	1	02	1	1	1	1
03	1	1	1	1	03	1	1	1	1
04	1	1	1	1	04	1	1	1	1
05	1	1	1	1	05	1	1	1	1
06	1	1	1	1	06	1	1	1	1
07	1	1	1	1	07	1	1	1	1
08	1	1	1	1	08	1	1	1	1
09	1	1	1	1	09	1	1	1	1
10	1	1	1	1	10	1	1	1	1
11	1	1	1	1	11	1	1	1	1
12	1	1	1	1	12	1	1	1	1
13	1	1	1	1	13	1	1	1	1
14	1	1	1	1	14	1	1	1	1
15	1	1	1	1	15	1	1	1	1
16	1	1	1	1	16	1	1	1	1
17	1	1	1	1	17	1	1	1	1
18	1	1	1	1	18	1	1	1	1
19	1	1	1	1	19	1	1	1	1
20	1	1	1	1	20	1	1	1	1
21	1	1	1	1	21	1	1	1	1
22	1	1	1	1	22	1	1	1	1
23	1	1	1	1	23	1	1	1	1
24	1	1	1	1	24	1	1	1	1
25	1	1	1	1	25	1	1	1	1
26	1	1	1	1	26	1	1	1	1
27	1	1	1	1	27	1	1	1	1
28	1	1	1	1	28	1	1	1	1
29	1	1	1	1	29	1	1	1	1
30	1	1	1	1	30	1	1	1	1
31	1	1	1	1	31	1	1	1	1
32	1	1	1	1	32	1	1	1	1
33	1	1	1	1	33	1	1	1	1
34	1	1	1	1	34	1	1	1	1
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49	1	1	1	1	49	1	1	1	1
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51	1	1	1	1	51	1	1	1	1
52	1	1	1	1	52	1	1	1	1
53	1	1	1	1	53	1	1	1	1
54	1	1	1	1	54	1	1	1	1
55	1	1	1	1	55	1	1	1	1
56	1	1	1	1	56	1	1	1	1
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58	1	1	1	1	58	1	1	1	1
59	1	1	1	1	59	1	1	1	1
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64	1	1	1	1	64	1	1	1	1
65	1	1	1	1	65	1	1	1	1
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67	1	1	1	1	67	1	1	1	1
68	1	1	1	1	68	1	1	1	1
69	1	1	1	1	69	1	1	1	1
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78	1	1	1	1	78	1	1	1	1
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80	1	1	1	1	80	1	1	1	1
81	1	1	1	1	81	1	1	1	1
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84	1	1	1	1	84	1	1	1	1
85	1	1	1	1	85	1	1	1	1
86	1	1	1	1	86	1	1	1	1
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91	1	1	1	1	91	1	1	1	1
92	1	1	1	1	92	1	1	1	1
93	1	1	1	1	93	1	1	1	1
94	1	1	1	1	94	1	1	1	1
95	1	1	1	1	95	1	1	1	1
96	1	1	1	1	96	1	1	1	1
97	1	1	1	1	97	1	1	1	1
98	1	1	1	1	98	1	1	1	1
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*** RESET AVERAGE 14:25:00 28 4.6 PPM
*** RESET AVERAGE 14:25:00 29 2.8 PPM
*** RESET AVERAGE 14:25:00 24 14.7 PPM
*** RESET AVERAGE 14:25:00 25 149.8 PPM
*** RESET AVERAGE 14:25:00 22 3.2 PPM
*** RESET AVERAGE 14:25:00 24 3.5 PPM

*** RESET AVERAGE 14:25:00 28 4.6 PPM
*** RESET AVERAGE 14:25:00 29 2.8 PPM
*** RESET AVERAGE 14:25:00 24 14.7 PPM
*** RESET AVERAGE 14:25:00 25 149.8 PPM
*** RESET AVERAGE 14:25:00 22 3.2 PPM
*** RESET AVERAGE 14:25:00 24 3.5 PPM

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*** RESET AVERAGE 14:25:00 24 14.7 PPM
*** RESET AVERAGE 14:25:00 25 149.8 PPM
*** RESET AVERAGE 14:25:00 22 3.2 PPM
*** RESET AVERAGE 14:25:00 24 3.5 PPM

THU 14:24:37

THU 14:24:37

1A 0 0 7 5 10 13 12 5 15 0 17 5 20 5 25 0 PCT

*** RESET AVERAGE 15:25:00 26 115.7 PPM
*** RESET AVERAGE 15:25:00 26 9.7 PPM
*** RESET AVERAGE 15:25:00 24 21.8 PPM
*** RESET AVERAGE 15:25:00 23 118.5 PPM
*** RESET AVERAGE 15:25:00 22 3.8 PPM
*** RESET AVERAGE 15:25:00 20 11.0 PPM

*** RESET AVERAGE 15:20:00 26 119.3 PPM
*** RESET AVERAGE 15:20:00 24 99.8 PPM
*** RESET AVERAGE 15:20:00 24 21.1 PPM
*** RESET AVERAGE 15:20:00 23 111.0 PPM
*** RESET AVERAGE 15:20:00 22 3.9 PPM
*** RESET AVERAGE 15:20:00 20 11.9 PPM

BRIDGE
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BRIDGE
2-1
CHANGING

153

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16
17
18

18

[illegible]

1

[illegible]

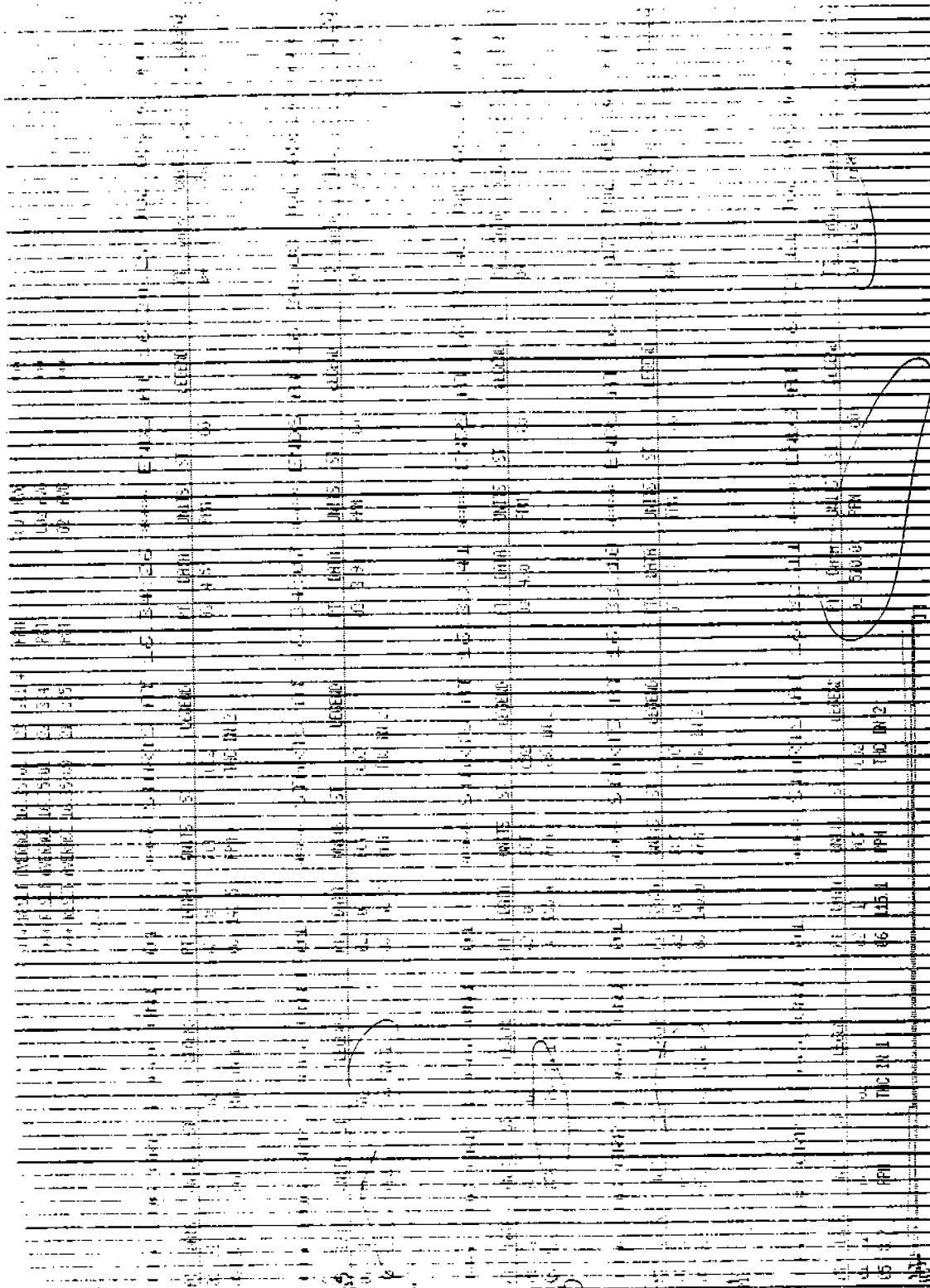
Year	1970	1971	1972	1973	1974	1975	1976	1977	1978	1979	1980	1981	1982	1983	1984	1985	1986	1987	1988	1989	1990	1991	1992	1993	1994	1995	1996	1997	1998	1999	2000	2001	2002	2003	2004	2005	2006	2007	2008	2009	2010	2011	2012	2013	2014	2015	2016	2017	2018	2019	2020	2021	2022	2023	2024	2025	2026	2027	2028	2029	2030	2031	2032	2033	2034	2035	2036	2037	2038	2039	2040	2041	2042	2043	2044	2045	2046	2047	2048	2049	2050	2051	2052	2053	2054	2055	2056	2057	2058	2059	2060	2061	2062	2063	2064	2065	2066	2067	2068	2069	2070	2071	2072	2073	2074	2075	2076	2077	2078	2079	2080	2081	2082	2083	2084	2085	2086	2087	2088	2089	2090	2091	2092	2093	2094	2095	2096	2097	2098	2099	2100
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[illegible]

	FEET	AVERAGE	SE	95% CI	P-VAL	COUNT
*** RESET AVERAGE	45:50.08	26	209.7	PMI	112.0	
*** RESET AVERAGE	45:50.08	25	112.8	PMI	106.0	

Abstract

22



STARTS AT 16:30:58				ENDS AT 16:31:58			
UNIT	DATA	UNIT	DATA	UNIT	DATA	UNIT	DATA
01	100.0	02	100.0	01	100.0	02	100.0
03	100.0	04	100.0	03	100.0	04	100.0
05	100.0	06	100.0	05	100.0	06	100.0
07	100.0	08	100.0	07	100.0	08	100.0
09	100.0	10	100.0	09	100.0	10	100.0
11	100.0	12	100.0	11	100.0	12	100.0
13	100.0	14	100.0	13	100.0	14	100.0
15	100.0	16	100.0	15	100.0	16	100.0
17	100.0	18	100.0	17	100.0	18	100.0
19	100.0	20	100.0	19	100.0	20	100.0
21	100.0	22	100.0	21	100.0	22	100.0
23	100.0	24	100.0	23	100.0	24	100.0
25	100.0	26	100.0	25	100.0	26	100.0
27	100.0	28	100.0	27	100.0	28	100.0
29	100.0	30	100.0	29	100.0	30	100.0
31	100.0	32	100.0	31	100.0	32	100.0
33	100.0	34	100.0	33	100.0	34	100.0
35	100.0	36	100.0	35	100.0	36	100.0
37	100.0	38	100.0	37	100.0	38	100.0
39	100.0	40	100.0	39	100.0	40	100.0
41	100.0	42	100.0	41	100.0	42	100.0
43	100.0	44	100.0	43	100.0	44	100.0
45	100.0	46	100.0	45	100.0	46	100.0
47	100.0	48	100.0	47	100.0	48	100.0
49	100.0	50	100.0	49	100.0	50	100.0
51	100.0	52	100.0	51	100.0	52	100.0
53	100.0	54	100.0	53	100.0	54	100.0
55	100.0	56	100.0	55	100.0	56	100.0
57	100.0	58	100.0	57	100.0	58	100.0
59	100.0	60	100.0	59	100.0	60	100.0
61	100.0	62	100.0	61	100.0	62	100.0
63	100.0	64	100.0	63	100.0	64	100.0
65	100.0	66	100.0	65	100.0	66	100.0
67	100.0	68	100.0	67	100.0	68	100.0
69	100.0	70	100.0	69	100.0	70	100.0
71	100.0	72	100.0	71	100.0	72	100.0
73	100.0	74	100.0	73	100.0	74	100.0
75	100.0	76	100.0	75	100.0	76	100.0
77	100.0	78	100.0	77	100.0	78	100.0
79	100.0	80	100.0	79	100.0	80	100.0
81	100.0	82	100.0	81	100.0	82	100.0
83	100.0	84	100.0	83	100.0	84	100.0
85	100.0	86	100.0	85	100.0	86	100.0
87	100.0	88	100.0	87	100.0	88	100.0
89	100.0	90	100.0	89	100.0	90	100.0
91	100.0	92	100.0	91	100.0	92	100.0
93	100.0	94	100.0	93	100.0	94	100.0
95	100.0	96	100.0	95	100.0	96	100.0
97	100.0	98	100.0	97	100.0	98	100.0
99	100.0	100	100.0	99	100.0	100	100.0

CH 1000
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*** RESET AVERAGE 17:40:00 26 115.4 PPM
*** RESET AVERAGE 17:40:00 25 110.0 PPM
*** RESET AVERAGE 17:40:00 24 26.5 PPM
*** RESET AVERAGE 17:40:00 23 216.1 PPM
*** RESET AVERAGE 17:40:00 22 4.1 PPM
*** RESET AVERAGE 17:40:00 21 1.7 PPM

75.0 100.0 125.0 150.0 175.0 200.0 225.0 250.0 PPM

*** RESET AVERAGE 17:35:00 26 117.1 PPM
*** RESET AVERAGE 17:35:00 25 110.5 PPM
*** RESET AVERAGE 17:35:00 24 25.4 PPM
*** RESET AVERAGE 17:35:00 23 246.3 PPM
*** RESET AVERAGE 17:35:00 22 1.7 PPM
*** RESET AVERAGE 17:35:00 21 1.7 PPM

*** RESET AVERAGE 17:30:00 26 111.8 PPM
*** RESET AVERAGE 17:30:00 25 117.2 PPM
*** RESET AVERAGE 17:30:00 24 28.4 PPM
*** RESET AVERAGE 17:30:00 23 204.9 PPM
*** RESET AVERAGE 17:30:00 22 4.1 PPM
*** RESET AVERAGE 17:30:00 21 1.7 PPM

*** RESET AVERAGE 17:25:00 26 119.0 PPM
*** RESET AVERAGE 17:25:00 25 117.2 PPM
*** RESET AVERAGE 17:25:00 24 28.4 PPM
*** RESET AVERAGE 17:25:00 23 204.9 PPM
*** RESET AVERAGE 17:25:00 22 4.1 PPM
*** RESET AVERAGE 17:25:00 21 1.7 PPM

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394 RW
396 RW
398 RW
400 RW

500 test set

1. *Chrysomelidae*
 2. *Chrysomelidae*
 3. *Chrysomelidae*
 4. *Chrysomelidae*

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126

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Figure 1: Schematic representation of the experimental design. The diagram shows a sequence of events: a subject is presented with a stimulus (a horizontal line with a dot), then a response is recorded (a horizontal line with a dot), and finally, the subject is presented with a stimulus (a horizontal line with a dot). The response is recorded again. The sequence is repeated for multiple trials. The diagram is labeled 'Figure 1' and 'Schematic representation of the experimental design'.

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2011-12 CH

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IN2	IN1	IN0	CD	ED2	ED1
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00	00	00	01	00	00
00	00	00	10	00	00
00	00	00	11	00	00
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00	00	01	10	00	00
00	00	01	11	00	00
00	01	00	00	00	00
00	01	00	01	00	00
00	01	00	10	00	00
00	01	00	11	00	00
00	01	01	00	00	00
00	01	01	01	00	00
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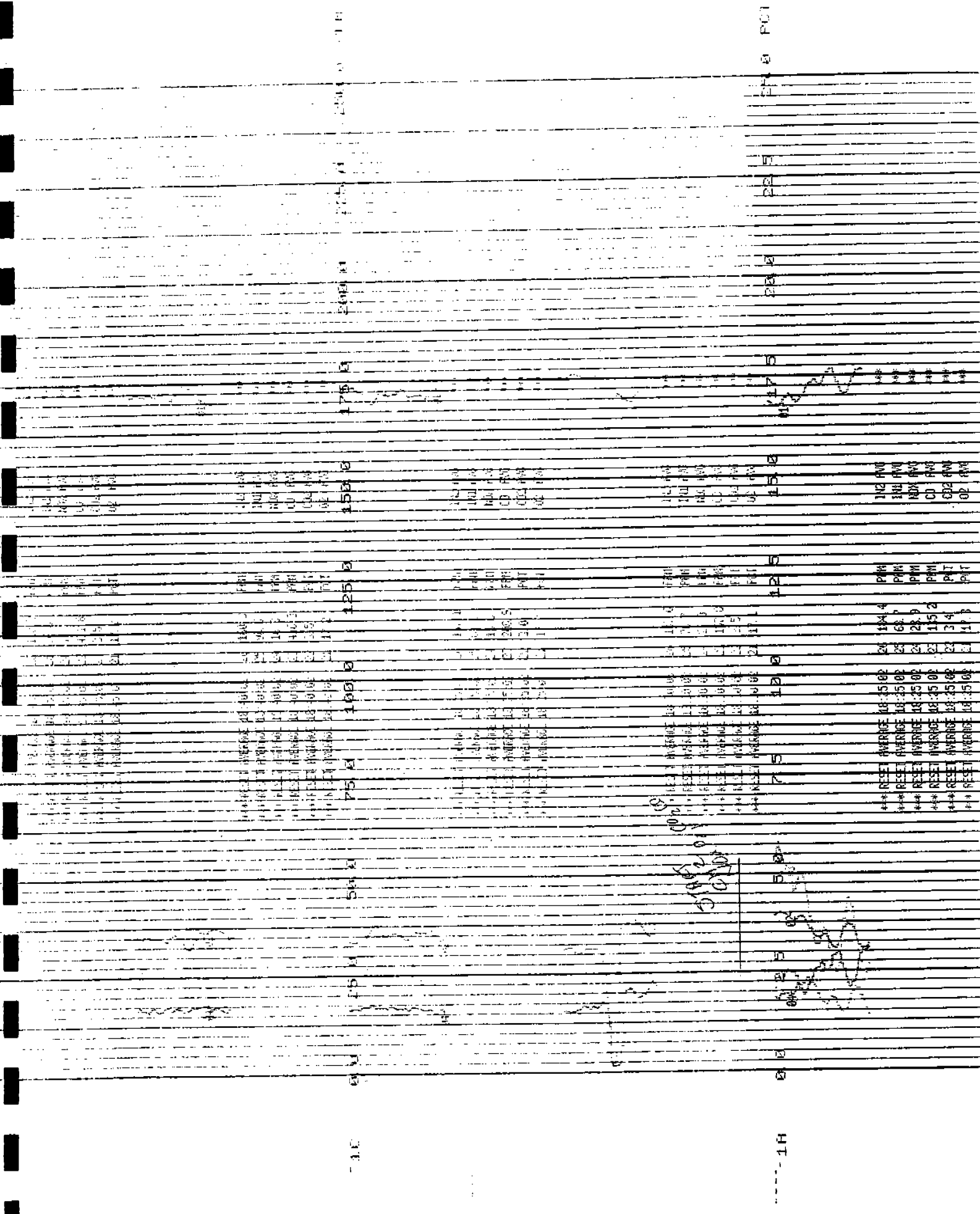
2.73	PWM
2.5	PWM
1.6	PWM
1.2	PWM
5	P&T
2.2	P&T

18:05:02	18:05:02	18:05:02	18:05:02	18:05:02	18:05:02
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RECEIVED
JUN 10 1964

1. The first step is to identify the key components of the system. This includes understanding the hardware, software, and data involved. For example, in a web application, this might involve identifying the server, database, and client-side code.

5-6-8



1H 2H 3H 4H 5H 6H 7H 8H 9H 10H 11H 12H 13H 14H 15H 16H 17H 18H 19H 20H 21H 22H 23H 24H 25H 26H 27H 28H 29H 30H 31H 32H 33H 34H 35H 36H 37H 38H 39H 40H 41H 42H 43H 44H 45H 46H 47H 48H 49H 50H 51H 52H 53H 54H 55H 56H 57H 58H 59H 60H 61H 62H 63H 64H 65H 66H 67H 68H 69H 70H 71H 72H 73H 74H 75H 76H 77H 78H 79H 80H 81H 82H 83H 84H 85H 86H 87H 88H 89H 90H 91H 92H 93H 94H 95H 96H 97H 98H 99H 100H

THY
P/O

CHCO
COA

Area
C/M
C/M

THY
P/O

DE GRP 1 LNI 01				STARTS AT 19:39:41				ENDS AT 19:39:42			
PT	UNIT	ST	LEGEND	PT	UNIT	ST	LEGEND	PT	UNIT	ST	LEGEND
42-1	PC	02		43-1	PC	02		44-1	PC	02	
05-1	PC	02		06-1	PC	02		07-1	PC	02	
08-1	PC	02		09-1	PC	02		10-1	PC	02	
11-1	PC	02		12-1	PC	02		13-1	PC	02	
14-1	PC	02		15-1	PC	02		16-1	PC	02	
17-1	PC	02		18-1	PC	02		19-1	PC	02	
20-1	PC	02		21-1	PC	02		22-1	PC	02	
23-1	PC	02		24-1	PC	02		25-1	PC	02	
26-1	PC	02		27-1	PC	02		28-1	PC	02	
29-1	PC	02		30-1	PC	02		31-1	PC	02	
32-1	PC	02		33-1	PC	02		34-1	PC	02	
35-1	PC	02		36-1	PC	02		37-1	PC	02	
38-1	PC	02		39-1	PC	02		40-1	PC	02	
41-1	PC	02		42-1	PC	02		43-1	PC	02	
44-1	PC	02		45-1	PC	02		46-1	PC	02	
47-1	PC	02		48-1	PC	02		49-1	PC	02	
50-1	PC	02		51-1	PC	02		52-1	PC	02	
53-1	PC	02		54-1	PC	02		55-1	PC	02	
56-1	PC	02		57-1	PC	02		58-1	PC	02	
59-1	PC	02		60-1	PC	02		61-1	PC	02	
62-1	PC	02		63-1	PC	02		64-1	PC	02	
65-1	PC	02		66-1	PC	02		67-1	PC	02	
68-1	PC	02		69-1	PC	02		70-1	PC	02	
71-1	PC	02		72-1	PC	02		73-1	PC	02	
74-1	PC	02		75-1	PC	02		76-1	PC	02	
77-1	PC	02		78-1	PC	02		79-1	PC	02	
80-1	PC	02		81-1	PC	02		82-1	PC	02	
83-1	PC	02		84-1	PC	02		85-1	PC	02	
86-1	PC	02		87-1	PC	02		88-1	PC	02	
89-1	PC	02		90-1	PC	02		91-1	PC	02	
92-1	PC	02		93-1	PC	02		94-1	PC	02	
95-1	PC	02		96-1	PC	02		97-1	PC	02	
98-1	PC	02		99-1	PC	02		100-1	PC	02	

CPN 1055

UNIT 1		UNIT 2		UNIT 3		UNIT 4		UNIT 5		UNIT 6		UNIT 7		UNIT 8		UNIT 9		UNIT 10		UNIT 11		UNIT 12		UNIT 13		UNIT 14		UNIT 15		UNIT 16		UNIT 17		UNIT 18		UNIT 19		UNIT 20		UNIT 21		UNIT 22		UNIT 23		UNIT 24		UNIT 25		UNIT 26		UNIT 27		UNIT 28		UNIT 29		UNIT 30		UNIT 31		UNIT 32		UNIT 33		UNIT 34		UNIT 35		UNIT 36		UNIT 37		UNIT 38		UNIT 39		UNIT 40		UNIT 41		UNIT 42		UNIT 43		UNIT 44		UNIT 45		UNIT 46		UNIT 47		UNIT 48		UNIT 49		UNIT 50		UNIT 51		UNIT 52		UNIT 53		UNIT 54		UNIT 55		UNIT 56		UNIT 57		UNIT 58		UNIT 59		UNIT 60		UNIT 61		UNIT 62		UNIT 63		UNIT 64		UNIT 65		UNIT 66		UNIT 67		UNIT 68		UNIT 69		UNIT 70		UNIT 71		UNIT 72		UNIT 73		UNIT 74		UNIT 75		UNIT 76		UNIT 77		UNIT 78		UNIT 79		UNIT 80		UNIT 81		UNIT 82		UNIT 83		UNIT 84		UNIT 85		UNIT 86		UNIT 87		UNIT 88		UNIT 89		UNIT 90		UNIT 91		UNIT 92		UNIT 93		UNIT 94		UNIT 95		UNIT 96		UNIT 97		UNIT 98		UNIT 99		UNIT 100	
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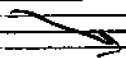


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CHART 1
SITES - Nos
344

CHART
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*** PRINTER OFF 09:22:14 JUL 09:95 ***

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100.0 PPM

20.0 PPM

1000.0 900.0 800.0 700.0 600.0 500.0 400.0 300.0 200.0 100.0 0.0

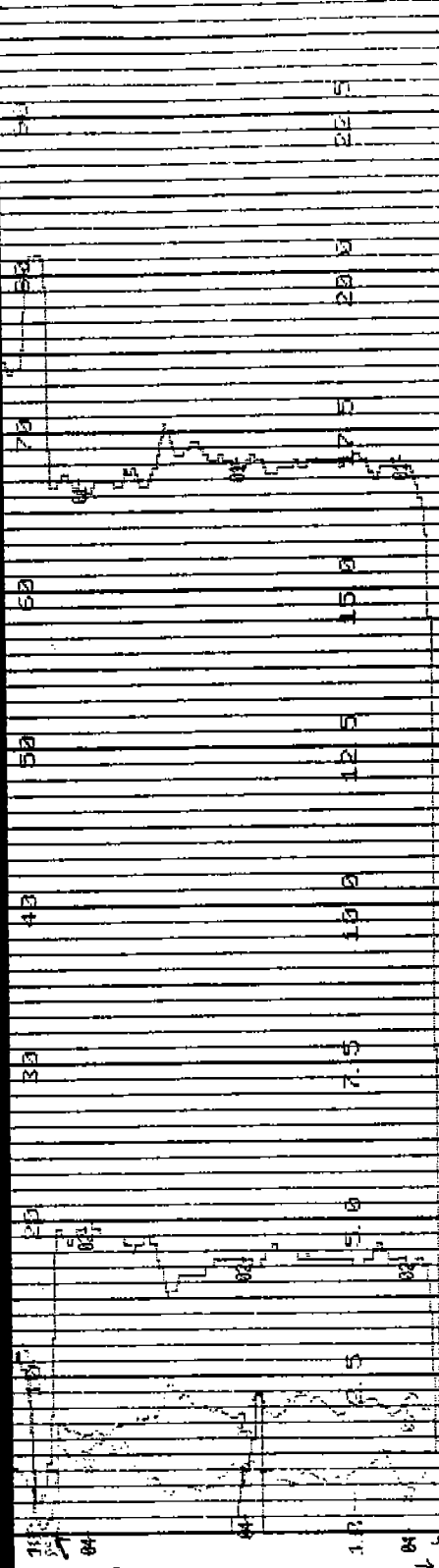
250.0 225.0 200.0 175.0 150.0 125.0 100.0 75.0 50.0 25.0 0.0

100.0 90 80 70 60 50 40 30 20 10 0

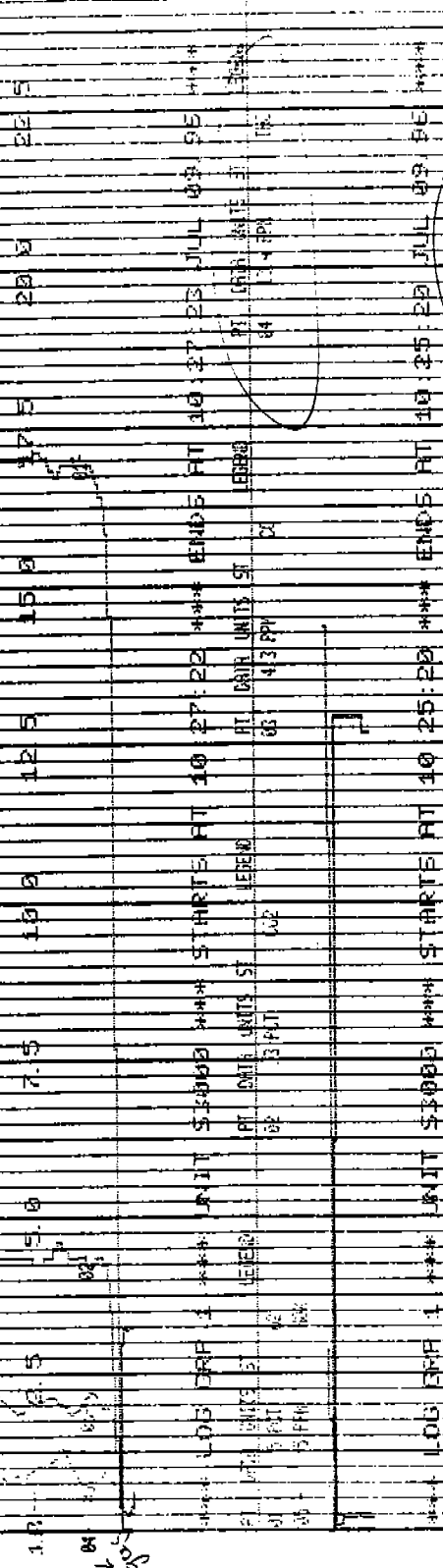
20.0 18.5 17.5 15.8 12.5 10.0 7.5 5.0 2.5 0.0

*** LOG ERP 1 *** UNIT 5000 *** STARTS RT 09 32:15 *** ENDS RT 09 32:25 JUL 02 95 ***
RT CRP UNITS ST LEBN
RT CRP UNITS ST LEBN

100 PPM



200 PPT



*** LOG TRF 1 *** UNIT 53000 *** STARTS AT 10:27:22 *** ENDS AT 10:27:23 JUL 09 95 ***

PT	DATA UNITS ST	LEGEND	PT	DATA UNITS ST	LEGEND
01	DATA UNITS ST	LEGEND	01	DATA UNITS ST	LEGEND
02	2 PPT	002	02	2 PPT	002
03	1.5 PPM	003	03	1.5 PPM	003
04	1.0 PPT	004	04	1.0 PPT	004

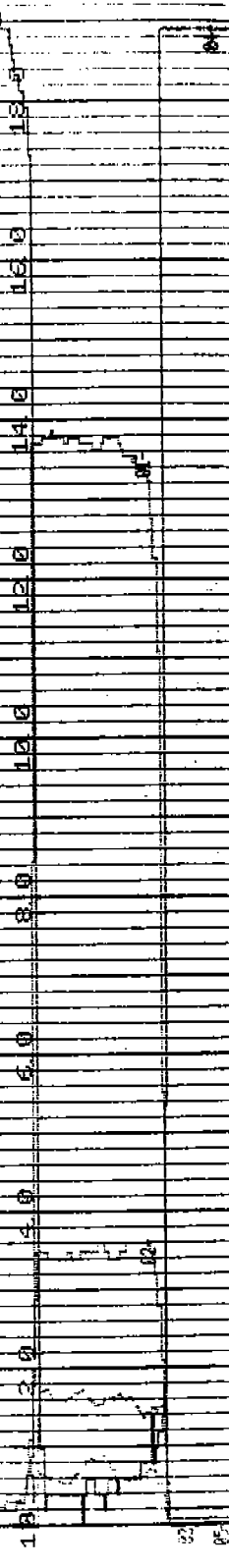
THC

THC

THC

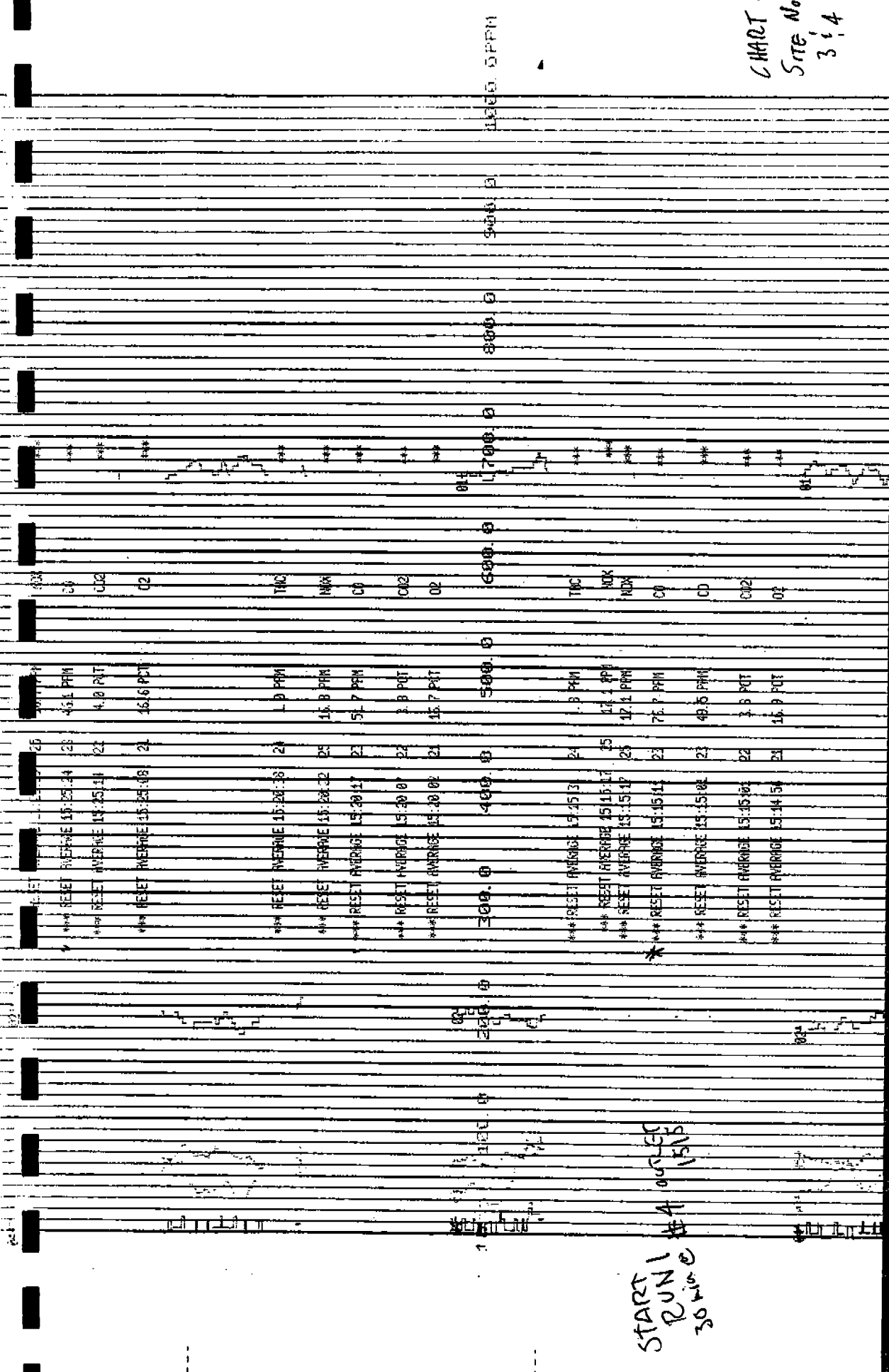
PT	DATA UNITS ST	LEGEND	PT	DATA UNITS ST	LEGEND
01	DATA UNITS ST	LEGEND	01	DATA UNITS ST	LEGEND
02	2 PPT	002	02	2 PPT	002
03	1.5 PPM	003	03	1.5 PPM	003
04	1.0 PPT	004	04	1.0 PPT	004

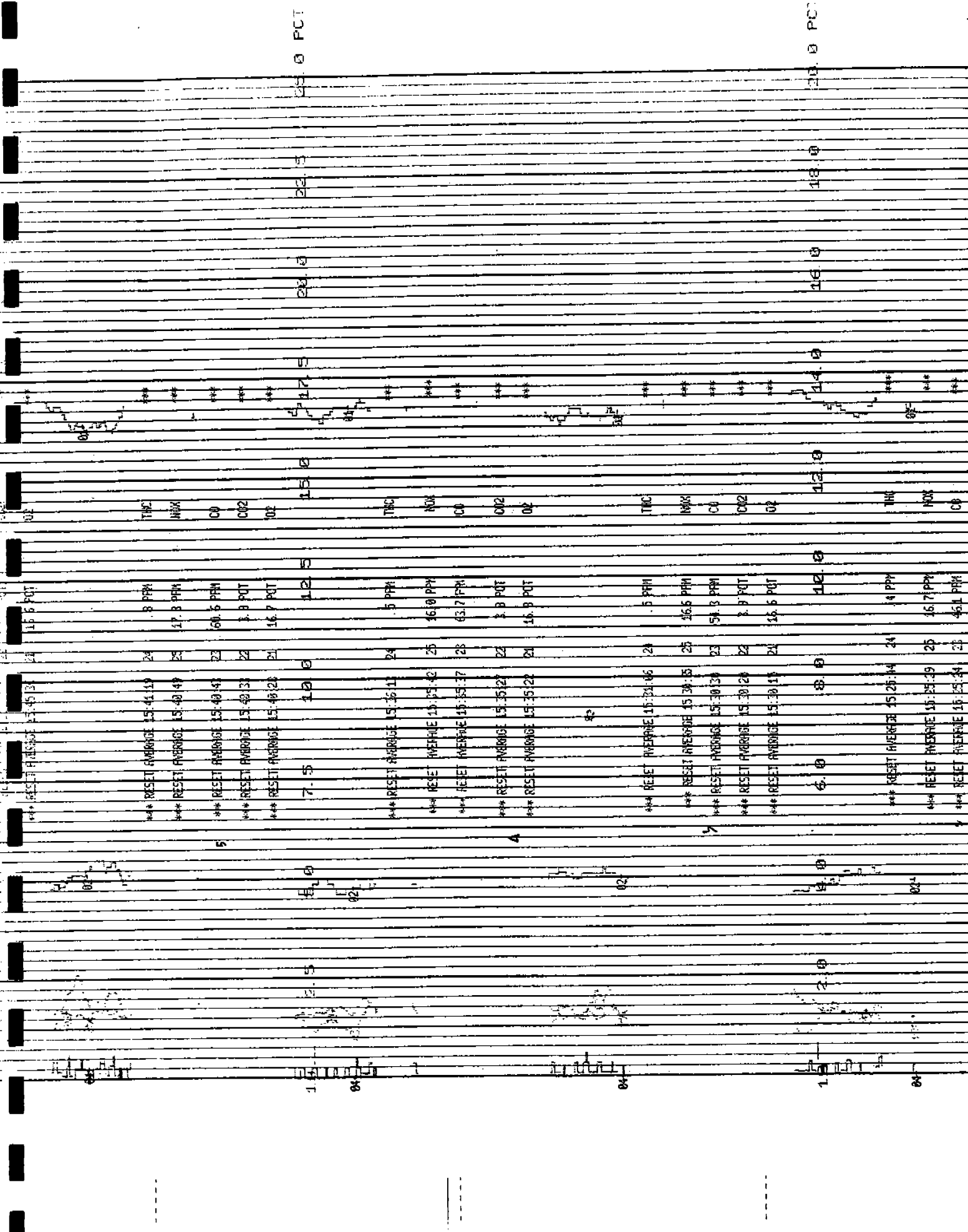
200 PPT



START RUN 1 #4 04550
30410

CHART 4
SITE Nos
3 & 4





*** RESET AVERAGE 15:45:31 24 15.5 PPM

*** RESET AVERAGE 15:40:49 25 17.8 PPM

*** RESET AVERAGE 15:40:41 23 16.5 PPM

*** RESET AVERAGE 15:40:31 22 1.8 PPM

*** RESET AVERAGE 15:40:21 21 16.7 PPM

7.5 12.5 15.0 20.0 22.5 25.0 PPM

*** RESET AVERAGE 15:35:11 24 5 PPM

*** RESET AVERAGE 15:35:42 25 16.0 PPM

*** RESET AVERAGE 15:35:37 28 63.7 PPM

*** RESET AVERAGE 15:35:27 22 3.8 PPM

*** RESET AVERAGE 15:35:22 21 16.8 PPM

6.0 10.0 12.0 14.0 16.0 18.0 PPM

*** RESET AVERAGE 15:30:06 24 5 PPM

*** RESET AVERAGE 15:30:35 25 16.6 PPM

*** RESET AVERAGE 15:30:30 23 51.3 PPM

*** RESET AVERAGE 15:30:20 22 3.9 PPM

*** RESET AVERAGE 15:30:11 21 16.5 PPM

6.0 10.0 12.0 14.0 16.0 18.0 PPM

*** RESET AVERAGE 15:25:14 24 4 PPM

*** RESET AVERAGE 15:25:19 25 16.7 PPM

*** RESET AVERAGE 15:25:14 23 46.1 PPM

*** RESET AVERAGE 15:25:11 21 4.0 PPM

6.0 10.0 12.0 14.0 16.0 18.0 PPM

NOT

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AA 500102
010102

*** LOG GRIP L *** UNIT 53000 *** STARTS AT 16:33:24 *** ENDS AT 16:38:25 JUL 09:56 ***

PT	DATA	UNITS	ST	LEGEND	PT	DATA	UNITS	ST	LEGEND
02	1.0	3.0	02	002	02	1.0	3.0	02	002
03	1.0	3.0	03	002	03	1.0	3.0	03	002
04	1.0	3.0	04	002	04	1.0	3.0	04	002
05	1.0	3.0	05	002	05	1.0	3.0	05	002
06	1.0	3.0	06	002	06	1.0	3.0	06	002
07	1.0	3.0	07	002	07	1.0	3.0	07	002
08	1.0	3.0	08	002	08	1.0	3.0	08	002
09	1.0	3.0	09	002	09	1.0	3.0	09	002
10	1.0	3.0	10	002	10	1.0	3.0	10	002
11	1.0	3.0	11	002	11	1.0	3.0	11	002
12	1.0	3.0	12	002	12	1.0	3.0	12	002
13	1.0	3.0	13	002	13	1.0	3.0	13	002
14	1.0	3.0	14	002	14	1.0	3.0	14	002
15	1.0	3.0	15	002	15	1.0	3.0	15	002
16	1.0	3.0	16	002	16	1.0	3.0	16	002
17	1.0	3.0	17	002	17	1.0	3.0	17	002
18	1.0	3.0	18	002	18	1.0	3.0	18	002
19	1.0	3.0	19	002	19	1.0	3.0	19	002
20	1.0	3.0	20	002	20	1.0	3.0	20	002
21	1.0	3.0	21	002	21	1.0	3.0	21	002
22	1.0	3.0	22	002	22	1.0	3.0	22	002
23	1.0	3.0	23	002	23	1.0	3.0	23	002
24	1.0	3.0	24	002	24	1.0	3.0	24	002
25	1.0	3.0	25	002	25	1.0	3.0	25	002
26	1.0	3.0	26	002	26	1.0	3.0	26	002
27	1.0	3.0	27	002	27	1.0	3.0	27	002
28	1.0	3.0	28	002	28	1.0	3.0	28	002
29	1.0	3.0	29	002	29	1.0	3.0	29	002
30	1.0	3.0	30	002	30	1.0	3.0	30	002
31	1.0	3.0	31	002	31	1.0	3.0	31	002
32	1.0	3.0	32	002	32	1.0	3.0	32	002
33	1.0	3.0	33	002	33	1.0	3.0	33	002
34	1.0	3.0	34	002	34	1.0	3.0	34	002
35	1.0	3.0	35	002	35	1.0	3.0	35	002

*** RESET AVERAGE 16:32:24 24 5.00 PM TNC

*** RESET AVERAGE 16:34:50 25 2.50 PM NOX

*** RESET AVERAGE 16:34:51 28 241.40 PM CO

*** RESET AVERAGE 16:34:51 22 5.50 PM CO2

*** RESET AVERAGE 16:34:51 21 5.90 PM CO2

*** RESET AVERAGE 16:34:51 21 5.90 PM CO2

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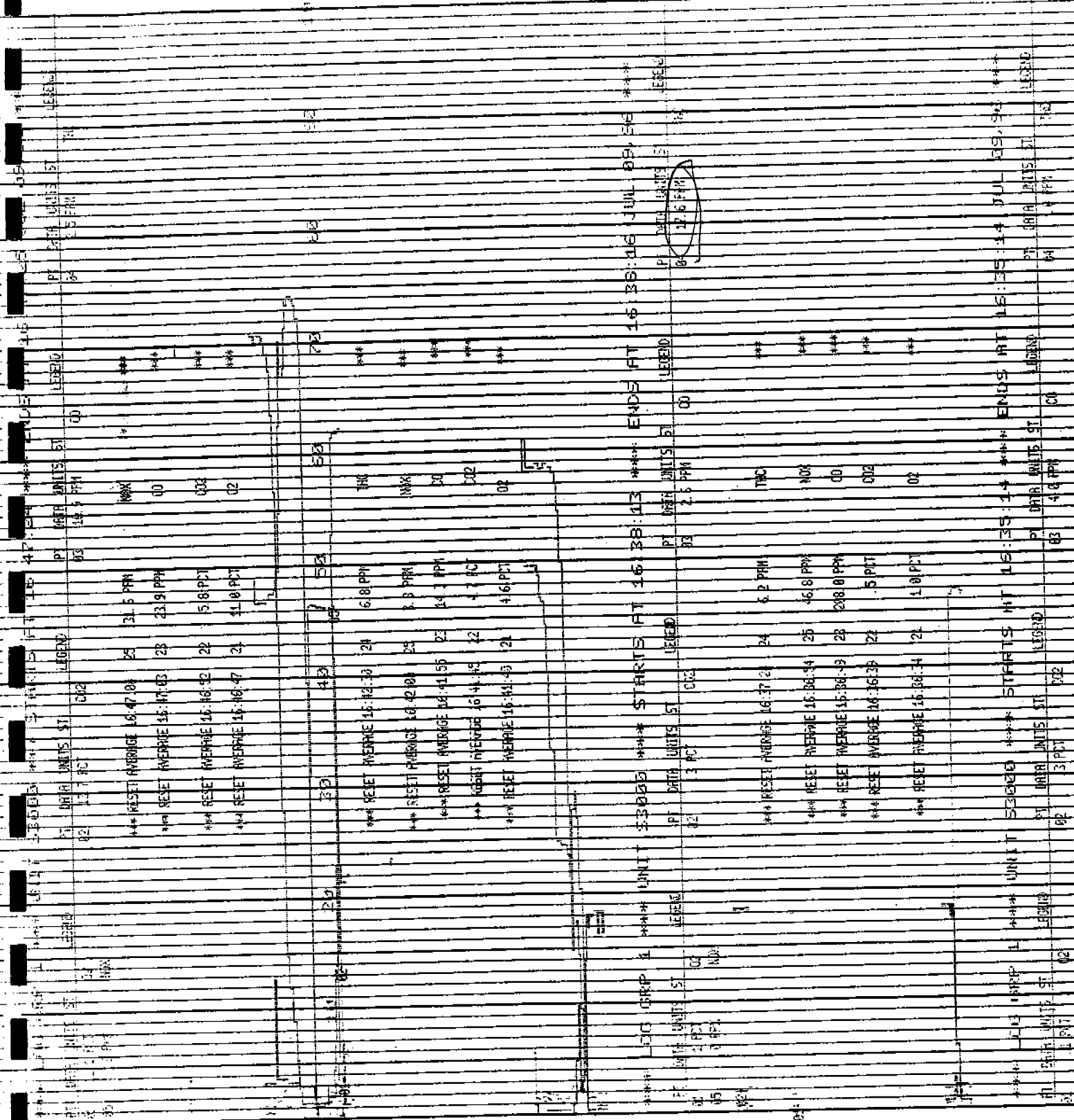
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LOG ORP 1 UNIT 3300 ***** STARTS AT 16:38:43 ***** ENDS AT 16:38:46 JUL 09, 98 *****

PT DATA UNITS ST LEGEND PT DATA UNITS ST LEGEND
02 1.1 PC 002 03 14.5 PPH 00
05 1.1 PPH 002 04 12.5 PPH 00

*** RESET AVERAGE 16:37:24 24 6.2 PPH TBC ***

*** RESET AVERAGE 16:36:34 25 46.8 PPH MAX ***

*** RESET AVERAGE 16:36:43 28 208.0 PPH 00 ***

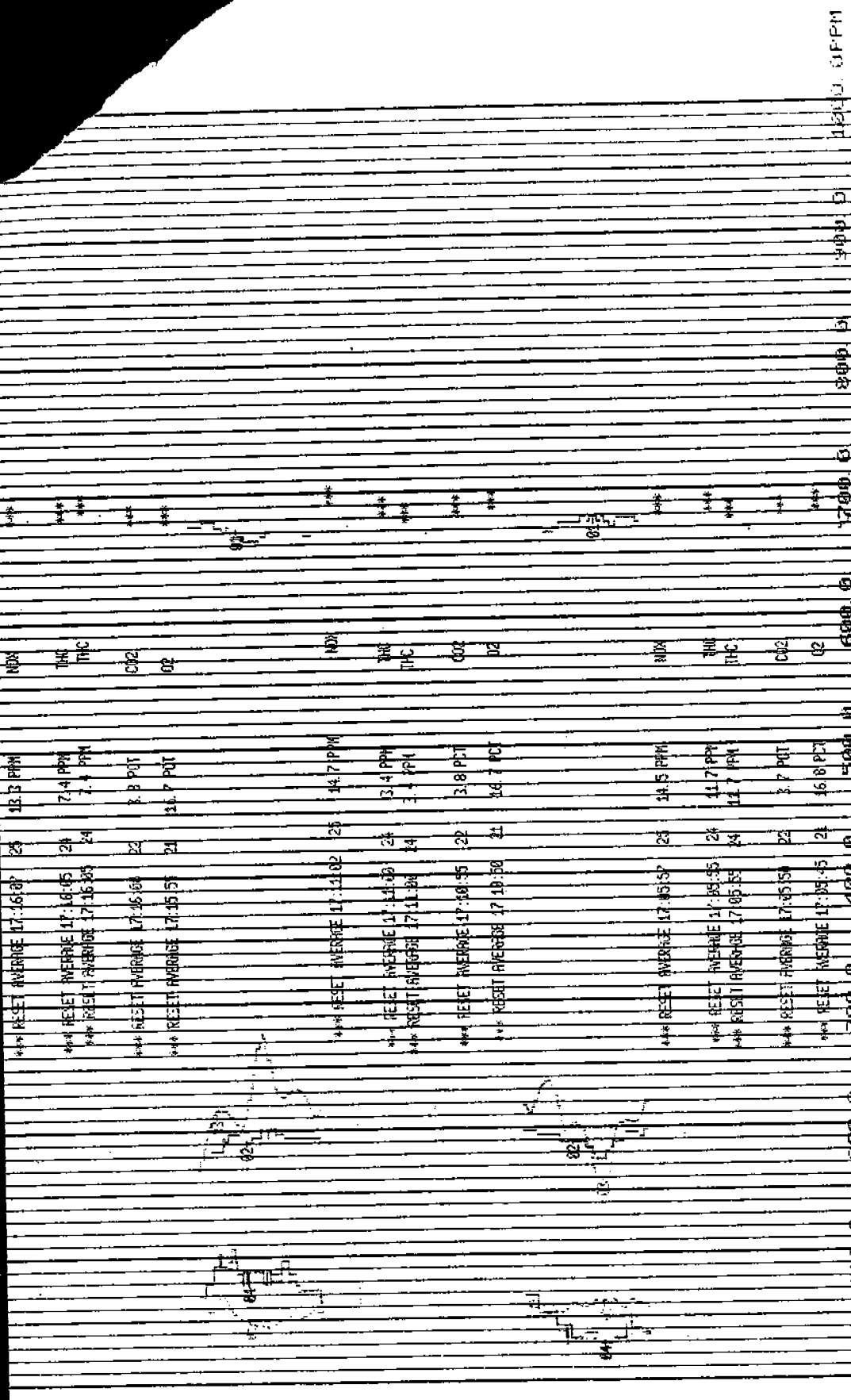
*** RESET AVERAGE 16:36:33 21 5 PPT 002 ***

*** RESET AVERAGE 16:36:34 21 1.0 PPT 02 ***

LOG ORP 1 UNIT 3300 ***** STARTS AT 16:35:14 ***** ENDS AT 16:35:14 JUL 09, 98 *****

PT DATA UNITS ST LEGEND PT DATA UNITS ST LEGEND
02 1.1 PPT 002 03 4.6 PPH 00
05 1.1 PPT 002 04 12.5 PPH 00

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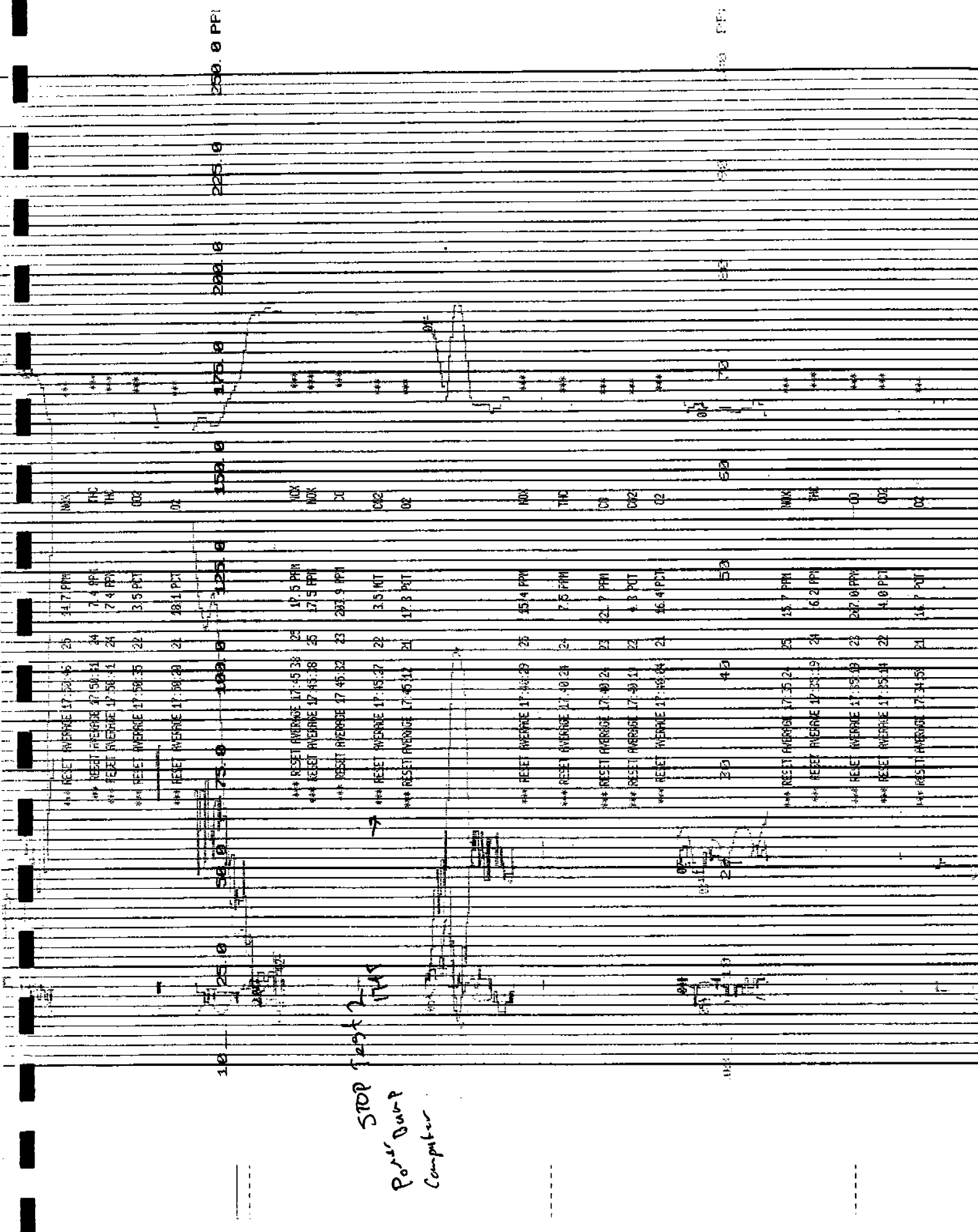
*** RESET AVERAGE 17:00:00	25	14.7 PPM	NOX
*** RESET AVERAGE 17:00:05	24	7.4 PPM	THC
*** RESET AVERAGE 17:00:10	24	7.4 PPM	THC
*** RESET AVERAGE 17:00:15	22	8.8 PPM	CO2
*** RESET AVERAGE 17:00:20	21	11.7 PPM	O2
*** RESET AVERAGE 17:00:25	26	14.7 PPM	NOX
*** RESET AVERAGE 17:00:30	24	13.4 PPM	THC
*** RESET AVERAGE 17:00:35	24	11.7 PPM	THC
*** RESET AVERAGE 17:00:40	22	13.8 PPM	CO2
*** RESET AVERAGE 17:00:45	21	16.7 PPM	O2
*** RESET AVERAGE 17:00:50	25	14.5 PPM	NOX
*** RESET AVERAGE 17:00:55	24	11.7 PPM	THC
*** RESET AVERAGE 17:01:00	24	11.7 PPM	THC
*** RESET AVERAGE 17:01:05	22	13.7 PPM	CO2
*** RESET AVERAGE 17:01:10	24	16.8 PPM	O2
*** RESET AVERAGE 17:01:15	25	14.2 PPM	NOX
*** RESET AVERAGE 17:01:20	25	14.2 PPM	NOX
*** RESET AVERAGE 17:01:25	24	13.8 PPM	THC
*** RESET AVERAGE 17:01:30	22	13.9 PPM	CO2
*** RESET AVERAGE 17:01:35	21	16.5 PPM	O2

Sheet 2 of 3

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*** RESET AVERAGE 17:30:20	15	14.1 PPM	NDX	17.5	20.0	22.5	25.0 PC
*** RESET AVERAGE 17:30:20	15	14.3 PPM	NDX	17.5	20.0	22.5	25.0 PC
*** RESET AVERAGE 17:30:15	23	204.1 PPM	00	17.5	20.0	22.5	25.0 PC
*** RESET AVERAGE 17:30:09	32	4.4 PC	003	17.5	20.0	22.5	25.0 PC
*** RESET AVERAGE 17:29:54	31	10.4 PC	02	17.5	20.0	22.5	25.0 PC
*** RESET AVERAGE 17:26:45	25	47.1 PPM	NDX	17.5	20.0	22.5	25.0 PC
*** RESET AVERAGE 17:26:16	34	6.7 PPM	TWC	17.5	20.0	22.5	25.0 PC
*** RESET AVERAGE 17:26:11	23	182.6 PPM	00	17.5	20.0	22.5	25.0 PC
*** RESET AVERAGE 17:26:11	23	182.6 PPM	00	17.5	20.0	22.5	25.0 PC
*** RESET AVERAGE 17:26:05	21	16.3 PPM	02	17.5	20.0	22.5	25.0 PC
*** RESET AVERAGE 17:21:19	23	14.3 PPM	NDX	17.5	20.0	22.5	25.0 PC
*** RESET AVERAGE 17:21:14	24	7.4 PPM	TWC	17.5	20.0	22.5	25.0 PC
*** RESET AVERAGE 17:21:06	21	209.7 PPM	00	17.5	20.0	22.5	25.0 PC
*** RESET AVERAGE 17:21:06	23	209.7 PPM	00	17.5	20.0	22.5	25.0 PC
*** RESET AVERAGE 17:21:00	21	17.0 PPM	02	17.5	20.0	22.5	25.0 PC

STOP Test 2
Power Dump
Computer



4	4.46	NET AVERAGE	18:13:24	25	18.6 PPM
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W. H. C. S. 1907

REFERENCE 18-25-5 339.3 pp4

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DATE RECEIVED 10-10-33 7.4 PM

[illegible]

106-15107-1

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100	100

[illegible]

444	RESE	AVERAGE	17.53	55	44.78941
-----	------	---------	-------	----	----------

[illegible]

NO. 4

8m
No. 4
10/10/10
20

15.0 PCT

UNIT 51000 STARTS AT 19:15:00 *** ENDS AT 19:15:01 JUL 89, 96 ***

PT DATA UNITS ST LEVND PT DATA UNITS ST LEVND

02 5 PCT 02 4.0 PCT 03 4.0 PCT 04 4.0 PCT

05 116.7 PCT 06 112.5 07 15.0 08 17.5 09 30.0 10 33.0

UNIT 53000 STARTS AT 19:13:38 *** ENDS AT 19:13:39 JUL 89, 96 ***

PT DATA UNITS ST LEVND PT DATA UNITS ST LEVND

02 1.0 PCT 03 1.0 PCT 04 1.0 PCT 05 1.0 PCT

06 1.0 PCT 07 1.0 PCT 08 1.0 PCT 09 1.0 PCT

10 1.0 PCT 11 1.0 PCT 12 1.0 PCT 13 1.0 PCT

UNIT 53000 STARTS AT 19:12:05 *** ENDS AT 19:12:05 JUL 89, 96 ***

PT DATA UNITS ST LEVND PT DATA UNITS ST LEVND

02 11.4 PCT 03 16.1 PCT 04 16.1 PCT 05 16.1 PCT

06 16.1 PCT 07 16.1 PCT 08 16.1 PCT 09 16.1 PCT

10 16.1 PCT 11 16.1 PCT 12 16.1 PCT 13 16.1 PCT

14 16.1 PCT 15 16.1 PCT 16 16.1 PCT 17 16.1 PCT

18 16.1 PCT 19 16.1 PCT 20 16.1 PCT 21 16.1 PCT

22 16.1 PCT 23 16.1 PCT 24 16.1 PCT 25 16.1 PCT

26 16.1 PCT 27 16.1 PCT 28 16.1 PCT 29 16.1 PCT

30 16.1 PCT 31 16.1 PCT 32 16.1 PCT 33 16.1 PCT

34 16.1 PCT 35 16.1 PCT 36 16.1 PCT 37 16.1 PCT

38 16.1 PCT 39 16.1 PCT 40 16.1 PCT 41 16.1 PCT

42 16.1 PCT 43 16.1 PCT 44 16.1 PCT 45 16.1 PCT

46 16.1 PCT 47 16.1 PCT 48 16.1 PCT 49 16.1 PCT

50 16.1 PCT 51 16.1 PCT 52 16.1 PCT 53 16.1 PCT

54 16.1 PCT 55 16.1 PCT 56 16.1 PCT 57 16.1 PCT

58 16.1 PCT 59 16.1 PCT 60 16.1 PCT 61 16.1 PCT

62 16.1 PCT 63 16.1 PCT 64 16.1 PCT 65 16.1 PCT

66 16.1 PCT 67 16.1 PCT 68 16.1 PCT 69 16.1 PCT

70 16.1 PCT 71 16.1 PCT 72 16.1 PCT 73 16.1 PCT

74 16.1 PCT 75 16.1 PCT 76 16.1 PCT 77 16.1 PCT

78 16.1 PCT 79 16.1 PCT 80 16.1 PCT 81 16.1 PCT

82 16.1 PCT 83 16.1 PCT 84 16.1 PCT 85 16.1 PCT

86 16.1 PCT 87 16.1 PCT 88 16.1 PCT 89 16.1 PCT

90 16.1 PCT 91 16.1 PCT 92 16.1 PCT 93 16.1 PCT

94 16.1 PCT 95 16.1 PCT 96 16.1 PCT 97 16.1 PCT

98 16.1 PCT 99 16.1 PCT 100 16.1 PCT 101 16.1 PCT

102 16.1 PCT 103 16.1 PCT 104 16.1 PCT 105 16.1 PCT

106 16.1 PCT 107 16.1 PCT 108 16.1 PCT 109 16.1 PCT

110 16.1 PCT 111 16.1 PCT 112 16.1 PCT 113 16.1 PCT

114 16.1 PCT 115 16.1 PCT 116 16.1 PCT 117 16.1 PCT

118 16.1 PCT 119 16.1 PCT 120 16.1 PCT 121 16.1 PCT

122 16.1 PCT 123 16.1 PCT 124 16.1 PCT 125 16.1 PCT

20.0 PCT

16.0

14.0

12.0

10.0

8.0

6.0

4.0

2.0

0.0

250.0 PPM

225.0

200.0

175.0

150.0

125.0

100.0

75.0

50.0

25.0

0.0

UNIT 53000 *** STARTS AT 19:35:41 *** ENDS AT 19:35:42 JUL 09:56 ***

PT DATA UNITS ST LEGEND PT DATA UNITS ST LEGEND PT DATA UNITS ST LEGEND

02 1.0 PPM 02 1.0 PPM 02 1.0 PPM

02 1.0 PPM 02 1.0 PPM 02 1.0 PPM

02 1.0 PPM 02 1.0 PPM 02 1.0 PPM

02 1.0 PPM 02 1.0 PPM 02 1.0 PPM

02 1.0 PPM 02 1.0 PPM 02 1.0 PPM

02 1.0 PPM 02 1.0 PPM 02 1.0 PPM

02 1.0 PPM 02 1.0 PPM 02 1.0 PPM

02 1.0 PPM 02 1.0 PPM 02 1.0 PPM

02 1.0 PPM 02 1.0 PPM 02 1.0 PPM

02 1.0 PPM 02 1.0 PPM 02 1.0 PPM

02 1.0 PPM 02 1.0 PPM 02 1.0 PPM

02 1.0 PPM 02 1.0 PPM 02 1.0 PPM

02 1.0 PPM 02 1.0 PPM 02 1.0 PPM

02 1.0 PPM 02 1.0 PPM 02 1.0 PPM

02 1.0 PPM 02 1.0 PPM 02 1.0 PPM

02 1.0 PPM 02 1.0 PPM 02 1.0 PPM

02 1.0 PPM 02 1.0 PPM 02 1.0 PPM

CO

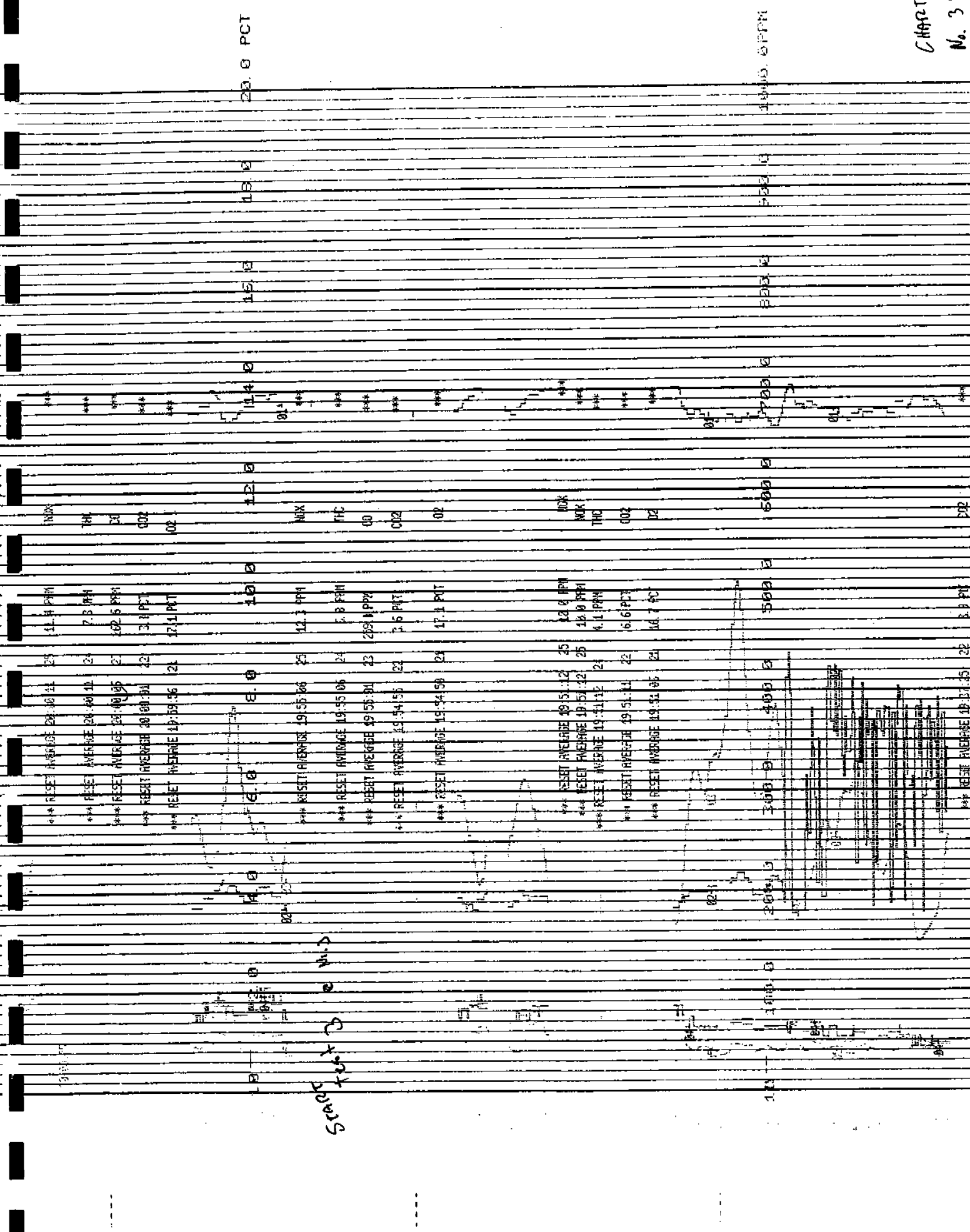
NO

CO

NO

5-13 B-7
No. 3

Chart
No. 35



1000.0 PPM

500.0

800.0

700.0

600.0

500.0

400.0

300.0

200.0

100.0

0.0

*** RESET AVERAGE 20:31:24 25 14.2 PPM

*** RESET AVERAGE 20:35:24 21 6.9 PPM

*** RESET AVERAGE 20:39:19 23 11.8 PPM

*** RESET AVERAGE 20:35:19 23 41.8 PPM

*** RESET AVERAGE 20:35:11 21 17.8 PPM

*** RESET AVERAGE 20:30:17 25 12.8 PPM

*** RESET AVERAGE 20:30:27 20 8.8 PPM

*** RESET AVERAGE 20:30:12 23 39.8 PPM

*** RESET AVERAGE 20:30:12 23 31.8 PPM

*** RESET AVERAGE 20:30:12 31 17.2 PPM

*** RESET AVERAGE 20:35:37 25 12.2 PPM

*** RESET AVERAGE 20:35:37 25 12.2 PPM

*** RESET AVERAGE 20:35:32 23 25.4 PPM

*** RESET AVERAGE 20:35:27 22 4.1 PPM

*** RESET AVERAGE 20:25:22 21 16.7 PPM

*** RESET AVERAGE 20:25:12 25 12.2 PPM

*** RESET AVERAGE 20:20:12 25 17.2 PPM

*** RESET AVERAGE 20:10:27 27 16.1 PPM

*** RESET AVERAGE 20:10:27 27 16.1 PPM

Swing No. 15

250.0 PPM

225.0

200.0

175.0

150.0

125.0

100.0

75.0

50.0

25.0

0.0

→ END 7850-3

WAX

THU

DI

00

02

NDX

THU

00

01

02

WAX

THU

DI

00

02

NDX

THU

DI

00

02

23.0 PCT

18.0

16.0

14.0

12.0

10.0

8.0

6.0

4.0

2.0

0.0

-2.0

-4.0

No. 3
Sys Bins

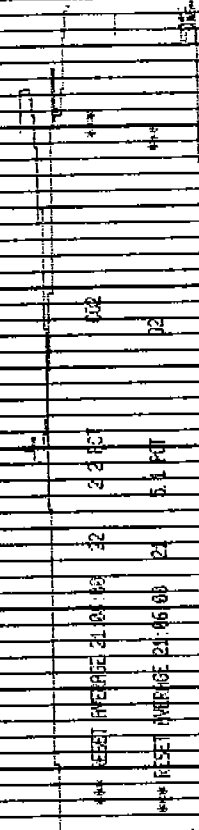
TAU

NOI

00

No. 4
Sys Bins

UNIT 50000 *** STARTS AT 21:08:06 *** ENDS AT 21:08:07 JUL 08/95 ***
PT DATA UNITS ST LEGEND
02 12.8 FCT 00 3.3 PM 04 5.0 PM 04 5.0 PM



UNIT 50000 *** STARTS AT 21:04:38 *** ENDS AT 21:04:39 JUL 08/95 ***
PT DATA UNITS ST LEGEND
02 1.0 FCT 00 3.5 PM 04 25.3 PM 04 25.3 PM

UNIT 50000 *** STARTS AT 21:03:20 *** ENDS AT 21:03:21 JUL 08/95 ***
PT DATA UNITS ST LEGEND
02 1.3 FCT 00 25.5 PM 04 0.7 PM 04 0.7 PM

UNIT 50000 *** STARTS AT 21:02:32 *** ENDS AT 21:02:33 JUL 08/95 ***
PT DATA UNITS ST LEGEND
02 1.0 FCT 00 42.8 PM 04 4.7 PM 04 4.7 PM

UNIT 50000 *** STARTS AT 21:00:56 *** ENDS AT 21:01:05 JUL 08/95 ***
PT DATA UNITS ST LEGEND
02 12.6 FCT 00 8.1 PM 04 9.4 PM 04 9.4 PM

UNIT 50000 *** STARTS AT 21:00:53 *** ENDS AT 21:00:53 JUL 08/95 ***
PT DATA UNITS ST LEGEND
02 12.6 FCT 00 8.1 PM 04 9.4 PM 04 9.4 PM

UNIT 50000 *** STARTS AT 21:00:52 *** ENDS AT 21:00:52 JUL 08/95 ***
PT DATA UNITS ST LEGEND
02 12.6 FCT 00 8.1 PM 04 9.4 PM 04 9.4 PM

UNIT 50000 *** STARTS AT 21:00:52 *** ENDS AT 21:00:52 JUL 08/95 ***
PT DATA UNITS ST LEGEND
02 12.6 FCT 00 8.1 PM 04 9.4 PM 04 9.4 PM

*** SYSTEM RESTART 21:35:16 JUL 08, 96 ***

*** PRINTER OFF 21:16:32 JUL 08, 96 ***

*** RESET AVERAGE 21:16:25 45.8 PPM NOX ***

*** RESET AVERAGE 21:35:16 24 6.5 PPM THO ***

*** RESET AVERAGE 21:15:11 23 288.5 PPM CO ***

*** RESET AVERAGE 21:06:11 23 288.5 PPM CO ***

*** RESET AVERAGE 21:06:11 21 5.5 PPM O2 ***

*** LOG OFF L *** UNIT 53000 *** STARTS AT 21:13:34 *** ENDS AT 21:13:36 JUL 08, 96 ***

PT DATA UNIT ST LEGND PT DATA UNIT ST LEGND PT DATA UNIT ST LEGND

02 12 PPM O2 08 37 PPM O2 04 3.8 PPM THO

02 148.5 PPM NOX 02 30 40 1.50 60 70 80 90 98

02 1.3 PPM CO2 02 3.8 PPM THO 02 3.8 PPM THO

*** LOG OFF L *** UNIT 53000 *** STARTS AT 21:11:34 *** ENDS AT 21:11:36 JUL 08, 96 ***

PT DATA UNIT ST LEGND PT DATA UNIT ST LEGND PT DATA UNIT ST LEGND

02 1.3 PPM CO2 02 3.8 PPM THO 02 3.8 PPM THO

02 1.3 PPM CO2 02 3.8 PPM THO 02 3.8 PPM THO

*** RESET AVERAGE 21:11:10 15 1.5 PPM NOX ***

*** RESET AVERAGE 21:11:10 24 5.5 PPM THO ***

*** RESET AVERAGE 21:11:06 23 86.8 PPM CO ***

*** RESET AVERAGE 21:11:06 23 86.8 PPM CO ***

*** RESET AVERAGE 21:11:06 21 11.4 PPM O2 ***

*** LOG OFF L *** UNIT 53000 *** STARTS AT 21:08:08 *** ENDS AT 21:08:07 JUL 08, 96 ***

PT DATA UNIT ST LEGND PT DATA UNIT ST LEGND PT DATA UNIT ST LEGND

DRYER JULY 9th, 1996

NOX,CO,VOC,CO2,O2

DATA TIME:	START=	15:10	END=	17:50	HOURS=	2.67
	START=	18:10	END=	21:00	HOURS=	2.83
					TOTAL=	<u>5.50</u>

BOARD WEIGHTS - LBS

average weights determined by taking every 25th untrimmed board (from press tapes)

7/16"		201.6 lb= average
per/peice	46.87	untrimmed
per/ 8' x 16'	187.48	mat weight

7.0% =trim %

PLANT PRODUCTION RATE

5.50 =hours during testing
95 =pressloads
1,140 =no. of 8'x16' boards produced (pressloads x 12 boards per load)
145,920 =volume produced in surface footage (pressloads x 8'x16'x12 openings)
170,245 =volume produced 3/8" basis (pressloads x 8'x16'x 12 openings x 1.1667)
213,732 =lbs of finished product (boards produced x weight of finished board)
38,860 =lbs of finished product per hour (lbs of finshed product / hours)
19.43 =tons of finished product per hour (lbs of finshed product per hour / 2000 lb)

FUEL BURNING RATE ESTIMATED BY DRY FUEL INPUT

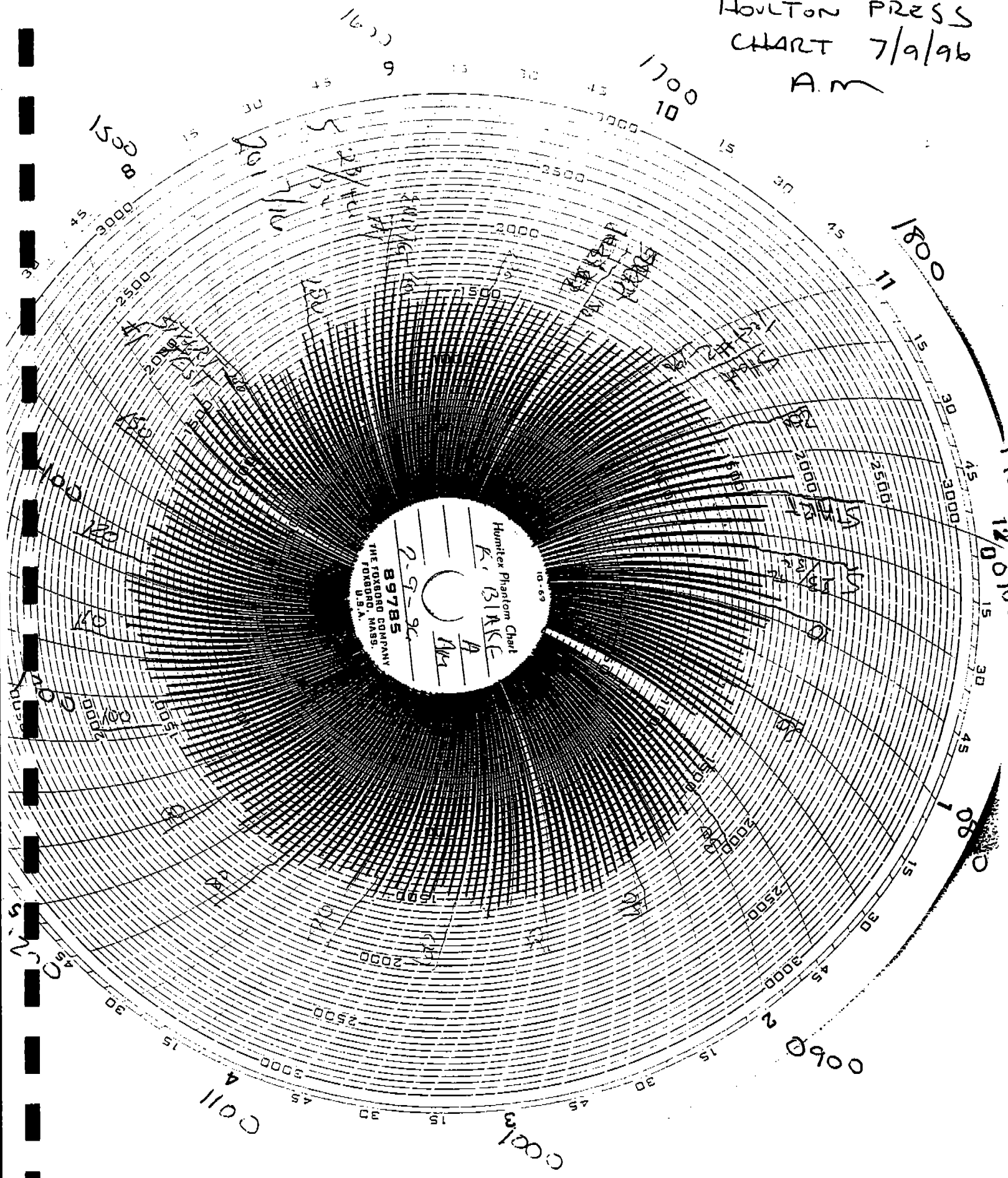
SURFACE

5.71 =SURFACE fuel calibration in pounds per count
2,811 =SURFACE counts during testing hours
16,051 =SURFACE lbs of fuel burned during testing
5.50 =hours during testing
2,918 =lbs of dry fuel burned per hour during testing (pounds of dry fuel / testing hours)
1.46 =tons of dry fuel burned per hour during testing (pounds of dry fuel / 2000 lbs)
8,500 =estimated BTU content per pound of dry fuel,
24.8 =estimated mmbtu input per hour (lbs of dry fuel per hour x btu content)
1,107 =average inlet temperature
33.05 =average incoming moisture percent
7.67 =average dry moisture percent

CORE

6.29 =CORE fuel calibration in pounds per count
2,464 =CORE counts during testing hours
15,499 =CORE lbs of fuel burned during testing
5.50 =hours during testing
2,818 =lbs of dry fuel burned per hour during testing (pounds of dry fuel / testing hours)
1.41 =tons of dry fuel burned per hour during testing (pounds of dry fuel / 2000 lbs)
8,500 =estimated BTU content per pound of dry fuel,
24.0 =estimated mmbtu input per hour (lbs of dry fuel per hour x btu content)
1,229 =average inlet temperature
33.05 =average incoming moisture percent
4.67 =average dry moisture percent

Houlton Press
Chart 7/9/96
A.M



P.m


$$18:10 - 21:00 = \underline{48}$$

955

Surf. 68 60.12

LINE SPEED	FROM	TO	THICK- NESS	PRESS LOADS	PRESS TEMP	OVERALL TIMER	DECOMP. TIMER	REASON FOR LINESPEED CHANGE
---------------	------	----	----------------	----------------	---------------	------------------	------------------	-----------------------------

$$5^{23/32} \pi = 14720$$
$$201 \quad 7/16 = 360202$$

206

(3/8" FOOTAGE) = 374.922

KONUS #1 0	KONUS #2 4288	SURFACE OIL BURNER 4/min	CORE OIL BURNER 0/min
------------	---------------	--------------------------	-----------------------

[illegible]

MOTOR #	FROM	TO	BRIEF DESCRIPTION OF WORK BEING DONE	INITIALS OF PERSON LOCKING OUT
LOCKED OUT				

TEST #1	3:15 to 4:20
---------	--------------

TEST #2

PRESS REPORT

LINE SPEED	FROM	TO	THICK- NESS	PRESS LOADS	PRESS TEMP	OVERALL TIMER	DECOMP. TIMER	REASON FOR LINESPEED CHANGE
---------------	------	----	----------------	----------------	---------------	------------------	------------------	-----------------------------

64	700	700	$\frac{7}{16}$	210	215°	140	12	Start
----	-----	-----	----------------	-----	------	-----	----	-------

TOTALS	210	(3/8" FOOTAGE) = 378.127 376.331
--------	-----	---

FLKR STROKES 1556 TDT 27 PEAB OIL BRNR: DEBARKER DT 1:57 SANDER DT 10:35

KONUS #1	KONUS #2 4217	SURFACE OIL BURNER	CORE OIL BURNER
----------	---------------	--------------------	-----------------

DOWNTIME		DOWNTIME(MINS)				REASON FOR DOWN TIME
FROM	TO	M	E	O	QC	

732	735			3	Working on core wax
803	808			5	Working on core wax
541	600	19			Power bump

*** MAINTENANCE / LOCK-OUT LOG ***

MOTOR #	FROM	TO	BRIEF DESCRIPTION OF WORK BEING DONE	INITIALS OF PERSON LOCKING OUT
LOCKED OUT				

LOUISIANA-PACIFIC
DULTON, MAINE

SHIFT OPERATING REPORT

SUPERVISOR Prescott

SHIFT

AM
PM

CREW A

DATE 7-9-96

PRESS OPERATION:

THICKNESS	PRESSLOADS	3/8" ITG	DOWNTIME (Mins)			
			M	E	O	QC
1/16	201	360202				
3/32	5	14720				
TOTAL	206	374922	3	8	4	

YARD OPERATIONS:

FIRE DUMP CLEANED	<u>3</u>	TIMES
TRUCKS USED DIRECT		TRUCKS
BARK TRUCKS LOADED		TRAILERS
MISCELLANEOUS		

KONUS FURNACE	HRS. FUEL USAGE WOOD	HRS. FUEL USAGE OIL
#1	0	
#2	12 Hour	

DRYER OPERATION:

	DRY FUEL USAGE LBS.	OIL FUEL USAGE HRS.	AVE. INLET TEMP	RUNNING TIME MINS.	DOWN TIME	AVG. WET MOISTURE	AVG. DRY MOISTURE	REASON FOR OIL USAGE
CORE	7,810	0	1153	718	2	43.4%	4.6%	NONE USED
SURFACE	8,420	41 minutes	1115	705	15	47.8%	7.6%	Water Short

# OF UNITS	1/4	5/16	3/8	7/16	15/32	1/2	19/32	23/32 T+G	OTHER
A				107				4+46 Pc	
1/2 UNITS									
U				17 Pc					
E & X				1 Pc					

LESS THAN 99.5%, WHY?

MAINTENANCE/LOCK-OUT LOG

ACTOR #	LOCKED OUT	FROM	TO	BRIEF DESCRIPTION OF WORK BEING DONE	INITIALS OF PERSON LOCKING OUT

PERSONNEL COMMENTS/CONCERNS:

SENT/TARDY	REASON	EXTRA PERSONNEL	REASON

LOUISIANA-PACIFIC
BOULTON, MAINE

SHIFT OPERATING REPORT

SUPVISOR T. Tower

SHIFT

AM

PM

CREW

DATE

7/9/96

PRESS OPERATION:

THICKNESS	PRESSLOADS	3/8" FTC	DOWNTIME (Mins)			
			M	E	O	QC
7/16						
TOTAL	210	376 33 1	19			8

YARD OPERATIONS:

FIRE DUMP CLEANED	0	TIMES
TRUCKS USED DIRECT		TRUCKS
BARK TRUCKS LOADED		TRAILERS
MISCELLANEOUS		

KONUS FURNACE	HRS. FUEL USAGE WOOD	HRS. FUEL USAGE OIL
#1	0	0
#2	12 hrs.	0

DRYER OPERATION:

	DRY FUEL USAGE LBS.	OIL FUEL USAGE HRS.	AVE. INLET TEMP	RUNNING TIME MINS.	DOWN TIME	AVG. WET MOISTURE	AVG. DRY MOISTURE	REASON FOR OIL USAGE
CORE	7720	0	1220	704	16	50.2%	5.0%	None here
SURFACE	8880	0	1160	704	16	46.0%	7.7%	None here

# OF UNITS	1/4	5/16	3/8	7/16	15/32	1/2	19/32	23/32	OTHER
A				112					
A 1/2 UNITS									
U				3 pcs					
E & X				48 pcs					

IF LESS THAN 99.5%, WHY?

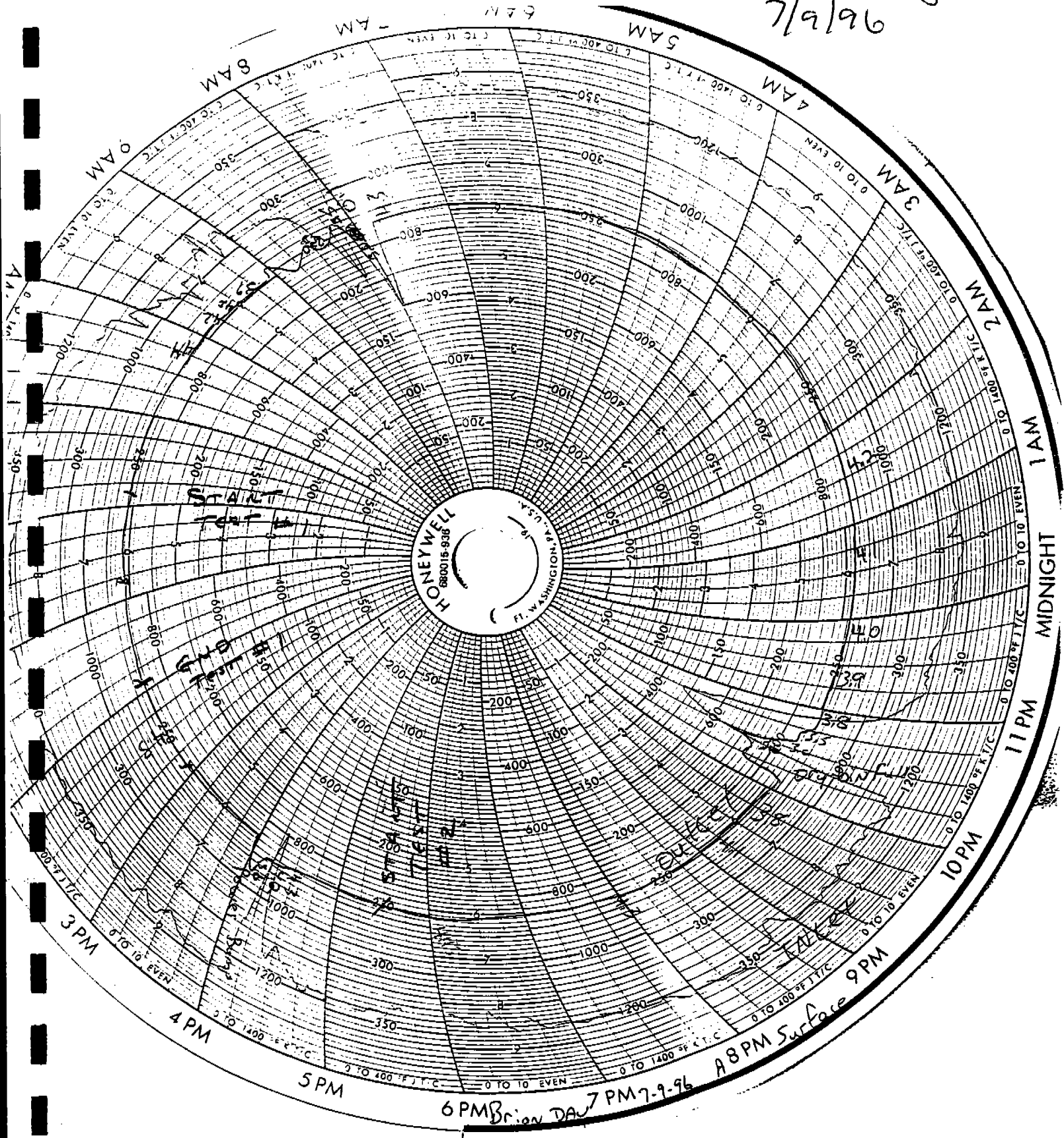
MAINTENANCE/LOCK-OUT LOG

MOTOR #	FROM	TO	BRIEF DESCRIPTION OF WORK BEING DONE	INITIALS OF PERSON LOCKING OUT
LOCKED OUT				

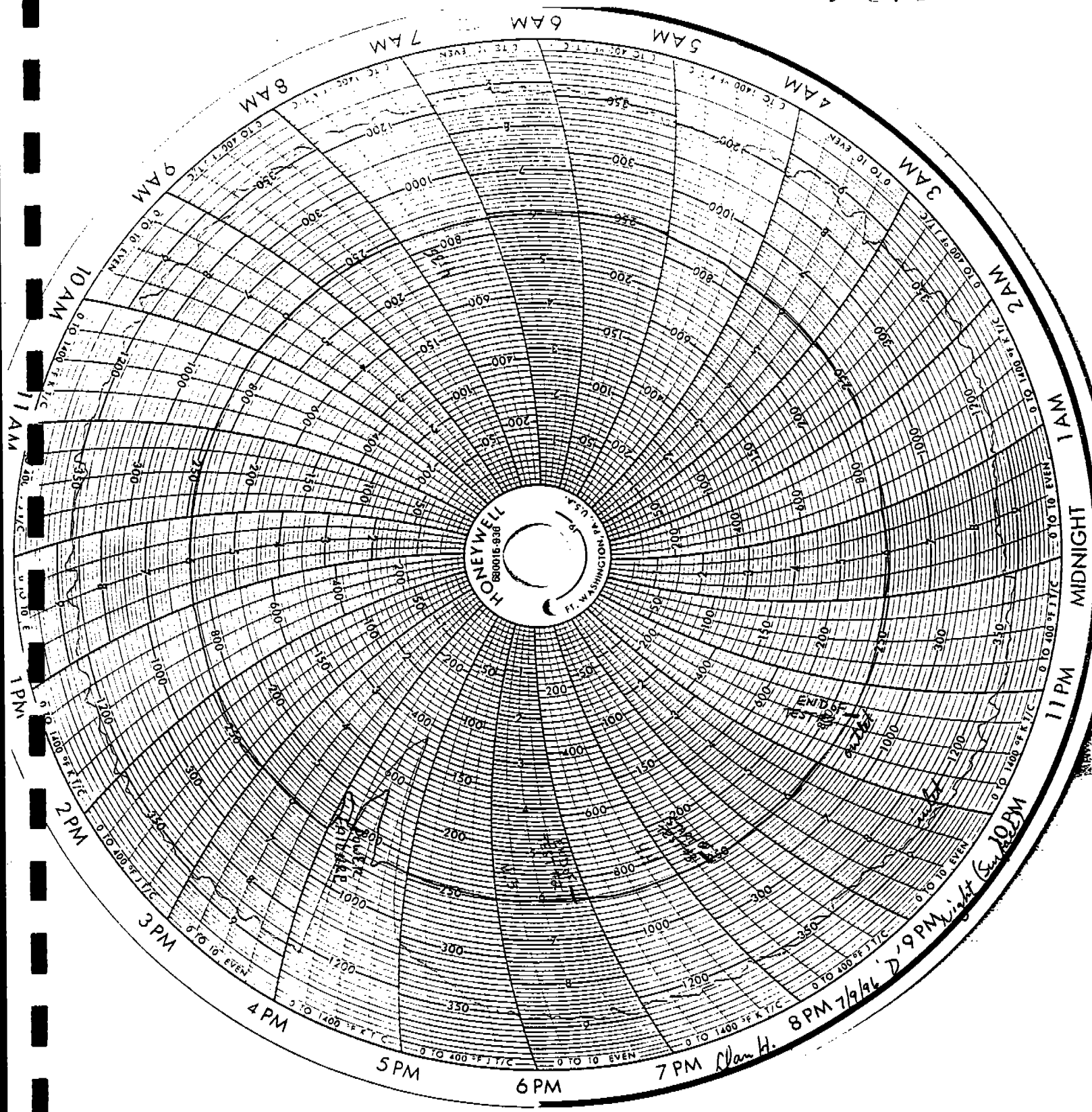
PERSONNEL COMMENTS/CONCERNS:

ABSENT/TARDY	REASON	EXTRA PERSONNEL	REASON

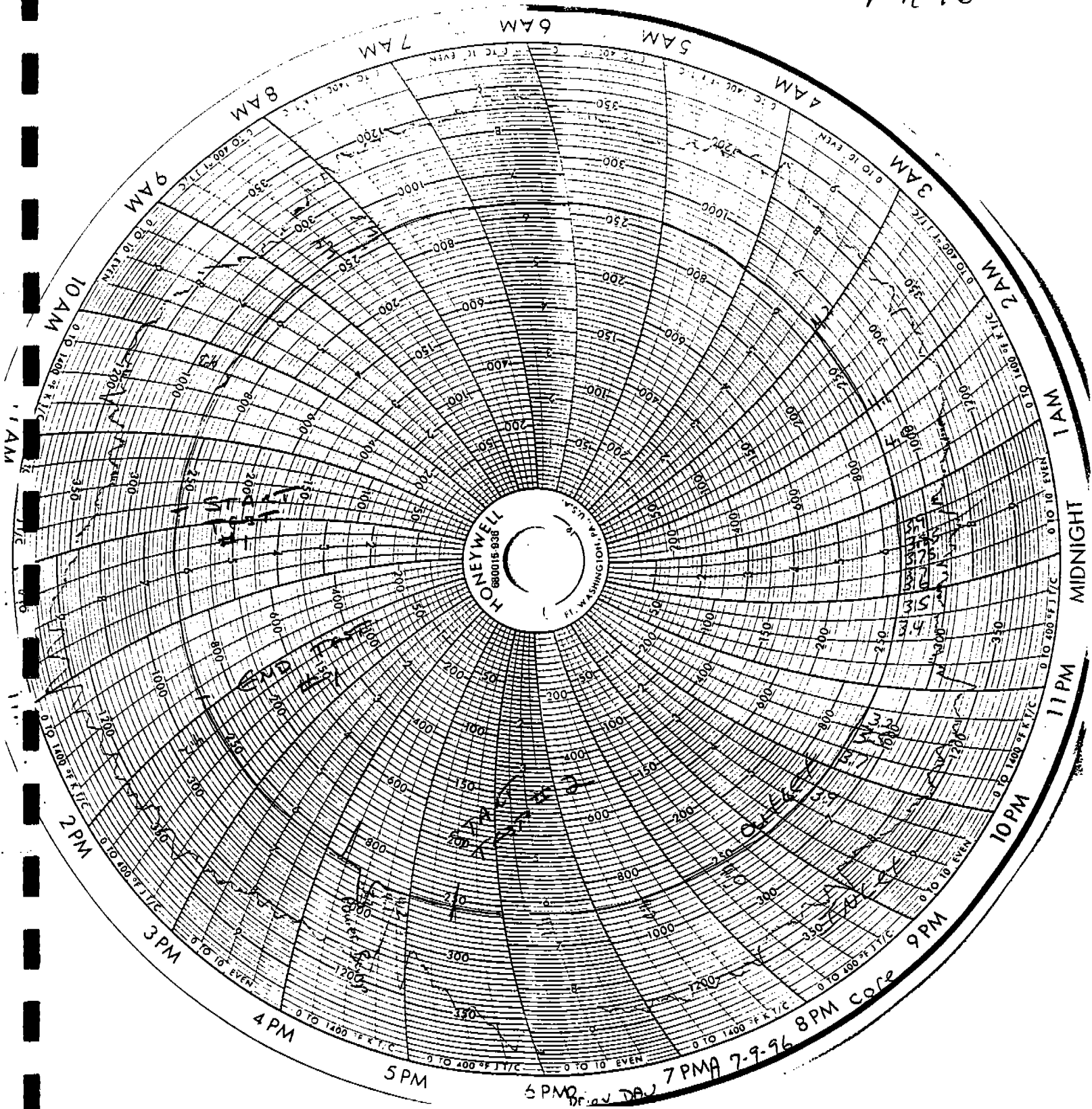
Houlton
SURFACE DRYER
7/9/96



HOUSTON
SURFACE DRYER
7/9/96

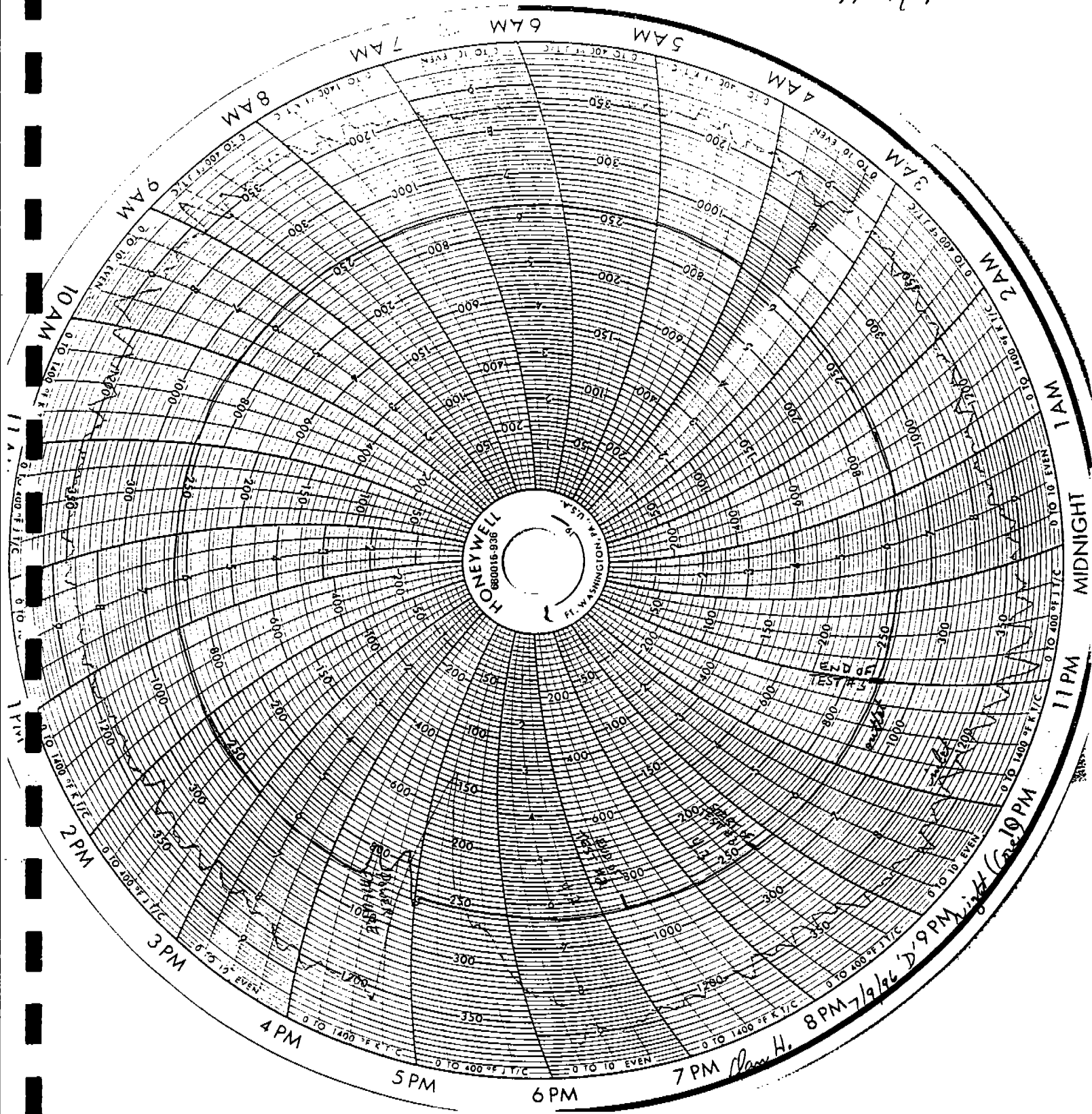


CORE DRYER
7/9/96



12/24.

Houlton
CORE DRYER
7/9/96



Brian / hence 7-9-96

DRYER READINGS - HOUTON

10 min TIME	FACE				CORE				DRY BIN		EVERY HOUR FLAKE MOISTURE					
	OUT. SET POINT	FEED RATE	INLET TEMP	OUTLET TEMP	FUEL COUNT	WET BIN LEVEL	FEED RATE	INLET TEMP	OUTLET TEMP	FUEL COUNT	WET BIN LEVEL	FACE	LEVEL	IN	FACE OUT	CORE OUT
8:00	242	4.3	1131	242.1	930	1/2+	4.0	1118	262.8	647	1/2+	3/1	3/1	43.4%	4.1%	4.5%
8:10	242	4.3	1132	242.2	946	1/2+	4.0	1166	261.0	822	1/2+	3/1	3/1			
8:20	242	4.1	1127	242.1	1046	1/2+	3.9	1193	266.0	931	1/2+	3/1	3/1			
8:30	243.5	4.1	1096	243.8	1198	1/2	3.9	1166	266.3	1016	1/2+	3/1	3/1			
8:40	245	3.8	1136	244.5	1316	1/2-	3.7	1173	262.2	1172	1/2-	3/1	3/1			
8:50	D R	VE R				1/2	3.5	1155	263.1	1160	1/2	3/1	3/1			
9:00	D R	VE R				1/2+	3.2	1043	265.4	1308	1/2+	3/1	3/1			
9:10	245	3.6	1019	245.0	1519	1/2+	3.2	1029	266.1	1396	1/2+	3/1	3/1	77.5%		4.4%
9:20	245	3.8	1050	245.3	1663	1/2+	3.2	1040	266.1	1523	1/2+	3/1	3/1			
9:30	245	3.9	1086	244.9	1774	1/2+	3.5	1052	264.3	1619	1/2+	3/1	3/1			
9:40	245	4.0	1118	245.1	1849	3/4-	3.6	1038	263.9	1710	3/4-	1/2	1/2			
9:50	245	4.0	1140	245.1	1996	3/4-	3.9	1065	263.4	1793	3/4-	1/2	1/2			
10:00	244	4.1	1112	244.2	2113	3/4-	3.9	1088	263.0	1878	3/4-	1/2	1/2	43.4%	7.0%	5.5%
10:10	244	4.1	1101	243.9	2237	3/4+	3.9	1132	262.9	1991	3/4+	1/2	1/2			
10:20	244	4.1	1112	244.0	2360	3/4-	3.9	1135	263.0	2101	3/4-	1/2	1/2			
10:30	244	4.1	1112	244.1	2490	3/4-	4.0	1159	263.0	2222	3/4-	1/2	1/2			
10:40	243	4.2	1143	243.4	2613	3/4	4.1	1168	263.2	2318	3/4	1/2	1/2			
10:50	243	4.2	1156	243.0	2734	1/2+	4.1	1156	263.1	2418	1/2+	1/2	1/2			
11:00	243	4.2	1148	242.9	2861	1/2	4.1	1147	262.8	2523	1/2	1/2	1/2			
11:10	243	4.2	1160	243.0	2940	1/2	4.2	1172	262.6	2636	1/2	1/2	1/2			
11:20	243	4.2	1148	243	3158	1/2	4.2	1170	262.5	2780	1/2	1/2	1/2	44.4%	7.2%	5.2%
11:30	243	4.2	1132	243.1	3268	1/2-	4.2	1202	263.7	2885	1/2	1/2	1/2			
11:40	243	4.2	1138	243.0	3381	1/2	4.2	1152	262.9	2983	1/2	1/2	1/2			
11:50	243	4.2	1141	243.1	3520	1/2	4.2	1138	262.9	3091	1/2	1/2	1/2			
12:00	243	4.2	1127	243.0	3640	1/2	4.2	1153	263.1	3175	1/2	1/2	1/2			
12:10	243	4.2	1117	243.1	3762	1/2+	4.2	1176	263.0	3306	1/2	1/2	1/2			
12:20	243	4.2	1107	242.8	3867	1/2	4.2	1203	262.8	3410	1/2	1/2	1/2			
12:30	243	4.2	1141	243.8	4008	1/2	4.2	1217	263.3	3540	1/2	1/2	1/2			
12:40	243	4.2	1139	243.8	4113	1/2-	4.2	1198	262.5	3641	1/2	1/2	1/2			
12:50	243	4.2	1162	243.6	4270	1/2	4.2	1177	262.5	3761	1/2	1/2	1/2			
1:00	243	4.2	1195	243.2	4470	1/2+	4.2	1190	262.3	3888	1/2	1/2	1/2			
1:10	243	4.2	1105	243.0	4546	1/2+	4.2	1171	263.0	3998	1/2	1/2	1/2			
1:20	243	4.2	1111	243.0	4645	1/2+	4.2	1166	263.0	4091	1/2	1/2	1/2			
1:30	243	4.2	1142	243.0	4807	1/2+	4.2	1196	263.0	4221	1/2	1/2	1/2			
1:40	D R	VE R				1/2	4.2	1070	262.9	4353	1/2	1/2	1/2			
1:50	243	4.2	856	243	4867	3/4-	4.2	1053	261.9	4397	1/2	1/2	1/2			
2:00	247	4.0	812	243	4967	3/4-	4.4	1144	262.2	4503	3/4-	1/2	1/2			

DRYER READINGS - HOULTON

TIME	FACE				CORE				WET BIN		DRY BIN		EVERY HOUR	
	OUT. SET	FEED	INLET	OUTLET	OUT. SET	FEED	INLET	OUTLET	FUEL	LEVEL	FACE	CORE	IN	FACE OUT
2:10	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4	45.6%	4.2%
2:20	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
2:30	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
2:40	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
2:50	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
3:00	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
3:10	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
3:20	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
3:30	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
3:40	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
3:50	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
4:00	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
4:10	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
4:20	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
4:30	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
4:40	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
4:50	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
5:00	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
5:10	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
5:20	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
5:30	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
5:40	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
5:50	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
6:00	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
6:10	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
6:20	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
6:30	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
6:40	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
6:50	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
7:00	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
7:10	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
7:20	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
7:30	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
7:40	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
7:50	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
8:00	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		
8:10	243	4.1	1108	243.3	262	4.1	1162	261.6	462	1/2	1/4	1/4		

Denny H. Love

Denny H. Love

2000

DRYER OPERATING REPORT

OPERATOR Brian

CREW D

SHIFT DAY

DATE 7/9/96

SURFACE DRYER

CORE DRYER

TIME	INLET	OUTPUT	FEED	OUTLET	INLET	DRY	TIME	INLET	OUTPUT	FEED	OUTLET	INLET	DRY	HAMMER
EVERY	MOIST	TEMP	SPEED	MOIST	TEMP	FUEL	EVERY	MOIST	TEMP	SPEED	MOIST	TEMP	FUEL	MILL
FOUR	%	%		CHAU	%	REV.	FOUR	%	%	%	CHAU	%	REV.	LOAD
7:00		241	4.45	8.0%	1130		7:00		259	4.4	4.4%	1200		35%
8:00		242	4.3	7.4%	1139	814	8:00		261	4.0	4.8%	1122	683	55%
9:00		Just started	5	Started	up	1387	9:00		266	3.2	4.4%	1034	1298	40%
10:00	47.8%	244	4.1	7.0%	1114	2096	10:00	43.4%	263	3.9	5.8%	1092	1871	45%
11:00		243	4.2	7.2%	1148	2874	11:00		263	4.1	5.2%	1165	2535	55%
12:00		243	4.2	8.0%	1123	3610	12:00		263	4.2	4.4%	1141	3177	50%
1:00		243	4.2	8.0%	1194	4381	1:00		263	4.2	4.8%	1189	3854	Full
2:00		247	4.0	9.0%	912	4862	2:00		262	4.4	4.2%	1190	4503	Full
3:00		243	4.4	6.6%	1082	5291	3:00		262	4.3	4.6%	1134	5132	35%
4:00		243	4.4	6.6%	1152	6140	4:00		262	4.3	4.6%	1248	5847	60%
5:00		243	4.4	7.0%	1157	6914	5:00		262	4.2	4.2%	1170	6518	40%
6:00		243	4.3	8.6%	1114	7720	6:00		262	4.2	4.2%	1149	7156	50%

10
3
2

2

COMMENTS AND REASONS FOR DOWNTIME:

8⁴⁷ Surface dryer down, Dry bin full
 4⁰ Surface dryer down⁽³⁾, woodfuel flame went out,
 4³ Started surface on oil, run oil 41 minutes and then back
 on woodfuel
 5⁴⁰ Both dryers down, Power Bump, 5⁴² Both dryers running

DRYER OPERATING REPORT

OPERATOR DAN H.

CREW D

SHIFT Night

DATE 7/9/96

SURFACE DRYER

CORE DRYER

INLET	OUTPUT	FEED	OUTLET	INLET	DRY	TIME	INLET	OUTPUT	FEED	OUTLET	INLET	DRY	HAMMER
MOIST	TEMP	SPEED	MOIST	TEMP	FUEL	EVERY	MOIST	TEMP	SPEED	MOIST	TEMP	FUEL	MILL
CHAU	%		CHAU	%	REV.	HOURLY	%	%	%	CHAU	%	REV.	LOAD
46.0%	243	4.3	7.6%	1180	E	7:00	50.2%	262	4.2	5.2%	1210	0	60%
	242	4.4	7.8%	1160	775	8:00		262	4.3	5.2%	1250	659	55%
	242	4.4	7.0%	1190	1558	9:00		262	4.3	5.2%	1330	1323	50%
	241	4.4	8.0%	1140	2434	10:00		262	4.3	4.4%	1160	2056	50%
	241	4.4	7.2%	1170	3099	11:00		261	4.3	5.2%	1230	2628	Fw11
	238	4.3	8.0%	1130	4137	12:00		261	4.3	6.8%	1220	3511	50%
	238	4.3	8.2%	1170	4776	1:00		261	4.3	5.0%	1240	4059	55%
	237	4.35	7.8%	1140	5708	2:00		261	4.3	4.4%	1290	4895	55%
	237	4.35	7.6%	1160	6249	3:00		261	4.3	4.6%	1210	5364	50%
	237	4.35	8.0%	1170	7060	4:00		261	4.3	4.2%	1160	6102	55%
	237	4.35	7.6%	1170	7716	5:00		261	4.3	5.6%	1130	6665	55%
STARTING BACK UP (POWERBUMP)						6:00	STARTING BACK UP (POWERBUMP) 50%						

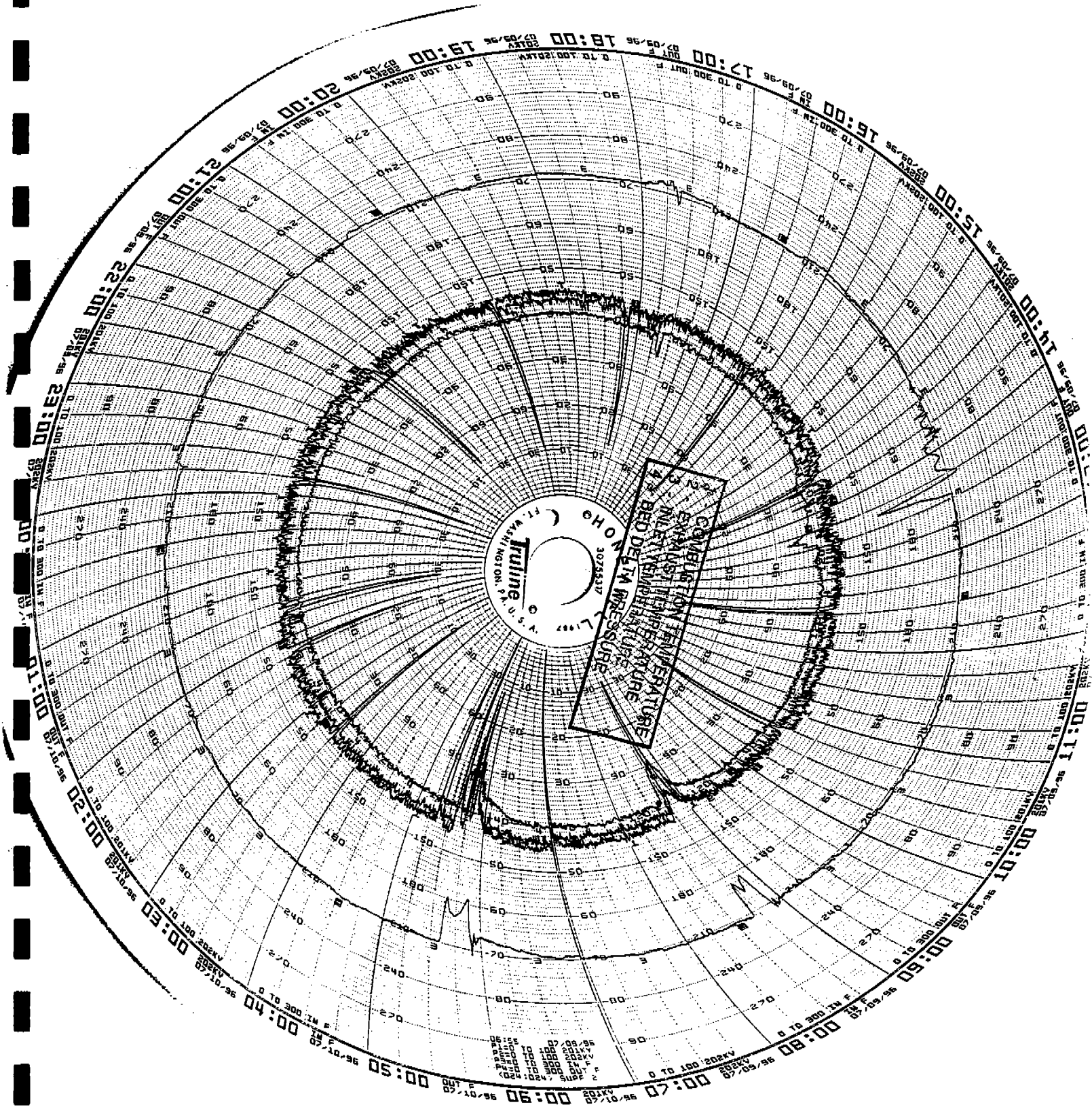
16

16

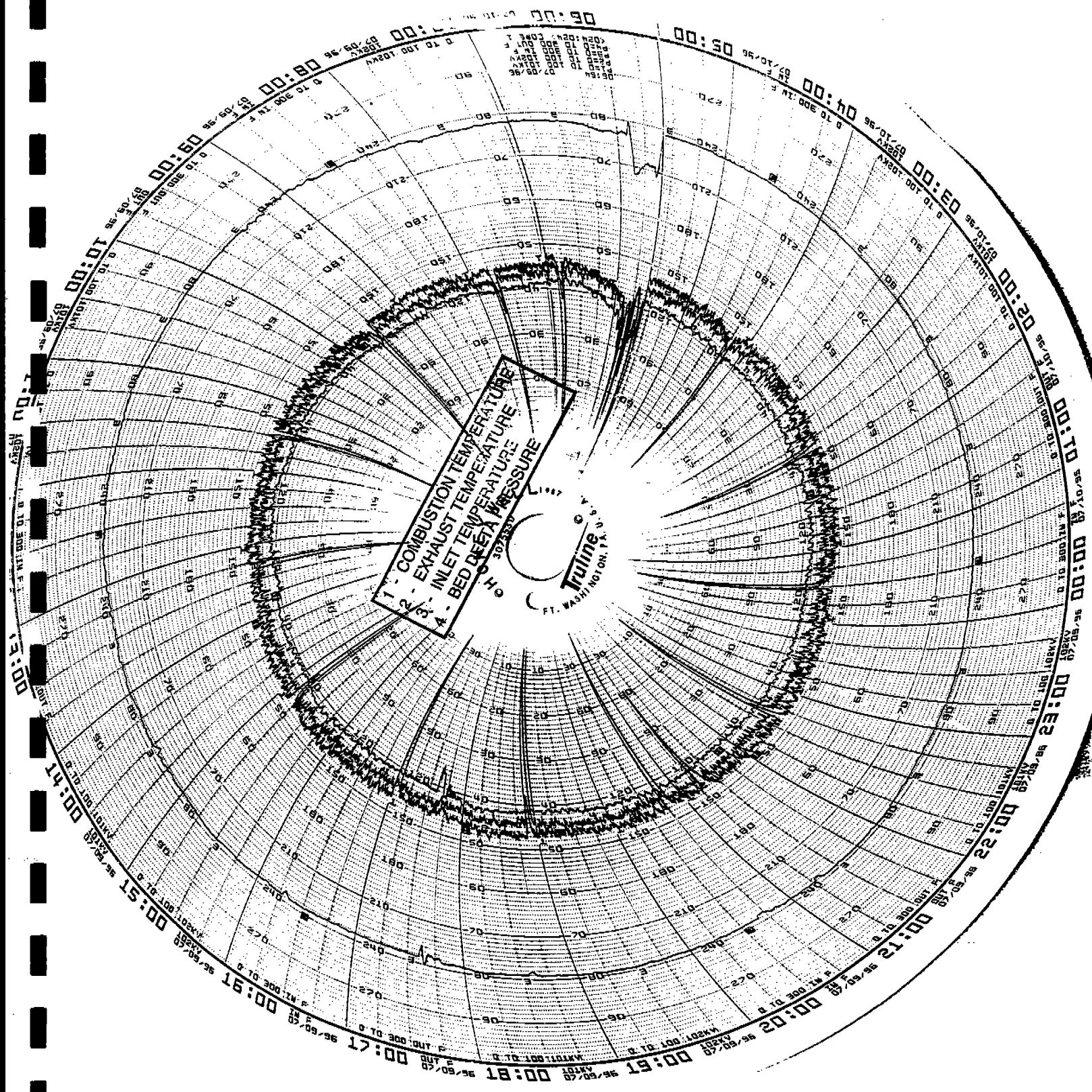
COMMENTS AND REASONS FOR DOWNTIME:

5:40 Powerbump, both dryers down.
5: Started both dryers.

HOUSTON 7/9/96
SURFACE E-TUBE



Horton 7/9/96
CORE - E-TUBE



E-tube Data Sheet

Houlton, Maine

Operator Brent Carmichael

Date 7/9 / 1996

Surface Unit												Core Unit											
T/R Set #101						T/R Set #102						T/R Set #201						T/R Set #202					
Time	mA	Kv	Spk/min	mA	Kv	Spk/min	Quench Inlet	Quench Outlet	PRESS	mA	Kv	Spk/min	mA	Kv	Spk/min	Quench Inlet	Quench Outlet	PRESS	Flush Time				
10:00	280	47	14.9	150	47	15.0	8	27		200	46	14.9	180	46	14.9	10	25						
10:10	210	46	15.0	155	46	14.9	8	27		210	47	14.9	125	46	14.9	10	25						
10:20	270	44	14.8	170	46	14.9	8	27		195	47	14.9	160	46	14.9	10	24						
10:30	250	46	14.9	180	45	14.9	9	27		210	48	14.9	180	44	14.9	10	26						
10:40	285	46	14.9	155	43	14.9	8	27		190	44	15.0	190	42	14.9	10	25		10:48-Surface				
10:50	190	47	15.0	190	43	14.9	8	27		209	44	16.4	187	45	14.9	10	24						
11:00	220	47	15.0	200	44	14.9	8	27		200	45	14.7	184	45	14.8	10	25						
11:10	210	46	15.0	195	43	14.9	8	27		210	44	14.7	180	45	14.8	10	25						
11:20	220	45	14.9	160	42	14.9	8	27		195	46	14.8	190	43	14.8	10	25						
11:30	260	46	14.8	150	42	14.9	8	28		210	43	14.9	190	42	15.0	10	25						
11:40	210	45	15.0	190	43	16.3	9	27		220	44	15.0	170	40	14.9	10	25		11:35-core				
11:50	200	46	14.9	190	43	14.7	8	27		225	43	14.8	150	42	14.9	10	25						
12:00	230	45	15.0	195	43	15.0	8	27		210	44	14.9	195	40	14.9	10	25						
12:10	235	46	14.8	210	47	14.9	8	27		230	47	14.9	205	44	14.8	10	25						
12:20	240	47	14.9	170	42	15.0	8	27		230	45	14.7	200	44	15.0	10	25						
12:30	250	47	14.9	190	43	14.9	8	27		220	43	14.9	190	41	15.0	10	25						
12:40	270	47	14.9	165	44	15.0	8	27		190	43	14.9	130	43	17.1	10	25		12:42-Surface				
12:50	240	45	14.9	130	44	14.8	9	27		185	45	14.9	125	43	14.9	10	25						
1:00	245	46	14.9	190	43	14.9	8	27		220	43	14.9	195	43	14.9	10	25						
1:10	280	49	26.5	190	44	25.2	9	27		220	44	23.7	245	43	24.7	10	25						
1:20	260	47	24.7	180	43	24.9	8	27		240	45	24.9	220	44	24.8	10	25						
1:30	240	46	30.5	210	44	24.8	9	27		210	43	24.8	200	44	24.9	10	25		12:6-core				
1:40	260	47	24.8	200	44	24.8	9	27		245	43	24.8	200	42	24.9	10	25						
1:50	300	49	24.8	220	45	24.9	8	27		400	48	24.7	260	43	24.6	10	26						

AM

PM

2

E-tube Data Sheet Houlton, Maine

Operator Brent Carmichael

Date 7/9 / 1996

Time	Core Unit										Surface Unit				
	T/R Set #101					T/R Set #102					T/R Set #201				
	mA	Kv	Spk/ min	mA	Kv	Spk/ min	Quench Inlet	Quench Outlet			mA	Kv	Spk/ min	Quench Inlet	Quench Outlet
2:00	260	48	29.9	170	43	30.0	8	27			360	43	29.9	320	43
2:10	250	47	29.8	200	43	29.9	9	27			370	44	29.9	270	44
2:20	235	48	29.8	260	43	29.8	8	27			340	46	29.6	340	45
2:30	270	46	30.1	190	44	29.8	9	27			120	11	30.5	250	46
2:40	265	48	29.7	190	43	29.9	8	27			210	44	31.0	225	42
2:50	300	49	29.8	185	42	29.8	8	27			240	46	29.8	260	42
3:00	265	47	29.8	180	43	29.9	8	27			260	46	29.8	180	43
3:10	270	46	29.8	230	43	30.0	9	27			240	43	29.9	250	42
3:20	280	48	30.0	240	45	30.8	9	27			240	45	29.8	200	43
3:30	285	47	29.9	860	44	29.9	9	27			225	44	29.9	190	42
3:40	280	47	29.7	220	45	29.8	9	27			270	43	29.9	180	43
3:50	240	46	30.0	220	44	29.9	8	27			210	45	29.8	190	43
4:00	270	48	29.8	170	45	29.9	8	27			250	44	30.0	190	44
4:10	255	49	29.9	180	45	29.8	9	27			280	45	29.8	180	42
4:20	260	47	29.7	220	46	29.8	8	27			220	44	29.8	240	47
4:30	265	50	29.7	220	43	29.9	9	27			215	45	29.7	180	44
4:40	260	48	30.0	215	43	29.8	8	27			230	44	29.9	180	43
4:50	225	47	30.0	190	45	30.0	9	27			190	44	29.8	240	44
5:00	250	46	29.7	210	44	29.8	8	27			240	44	29.8	210	43
5:10	280	46	30.8	200	44	29.8	8	27			240	45	29.9	200	44
5:20	260	48	30.0	200	46	30.0	8	27			240	46	29.8	200	44
5:30	220	46	29.7	200	45	29.8	8	27			250	45	29.8	200	46
5:40	220	45	29.6	210	44	29.7	8	27			240	44	29.7	220	43
5:50	280	50	29.9	240	46	29.8	8	27			220	46	29.8	220	47

50 face

315 code

END TEST 1

Surface

TEST 2 5:30

END TEST 2

PM

22

E-tube Data Sheet

Houlton, Maine

JOE CHARETTE
Operator Brent Goff Michael

Date 7 / 9 / 1996

Core Unit										Surface Unit										
Time	T/R Set #101					T/R Set #102					T/R Set #201					T/R Set #202				
	mA	Kv	Spk/ min	mA	Kv	Spk/ min	Quench Inlet	Quench Outlet	Press	mA	Kv	Spk/ min	mA	Kv	Spk/ min	Quench Inlet	Quench Outlet	Flush Time		
6:00	300	47	29.7	200	46	29.7	8	27		220	46	29.7	218	43	29.8	10	25			
6:10	290	50	29.7	220	46	29.7	8	27		230	44	30.0	240	46	29.8	10	25			
6:20	280	48	29.5	180	43	29.7	8	27		280	47	30.8	180	44	29.7	9	25			
6:30	260	50	29.8	170	46	29.8	8	27		240	47	29.7	200	45	29.7	9	25			
6:40	250	47	29.9	180	44	29.7	8	27		250	46	30.0	220	46	29.8	9	25			
6:50	260	47	29.8	220	46	29.8	8	27		200	44	29.8	200	44	29.8	9	25	658		
7:06	280	50	30.1	170	42	31.8	9	27		200	45	29.9	260	46	29.7	10	25			
7:10	200	46	29.7	210	46	29.7	9	27		180	44	29.8	280	47	29.7	10	25			
7:50	280	50	29.8	220	47	29.8	9	27		260	48	29.7	240	48	29.8	10	25			
8:00	260	48	29.7	180	45	30.1	9	27		260	45	29.9	220	47	30.0	10	25	2080		
8:10	260	48	29.8	220	46	30.0	9	27		250	44	29.8	200	46	29.8	10	25			
8:20	280	47	30.0	210	47	29.8	9	27		220	46	29.9	220	42	29.7	10	25			
8:30	250	50	29.8	200	46	28.9	9	27		250	47	30.0	200	44	29.7	10	25			
8:40	280	49	29.8	190	46	29.7	9	27		240	47	29.9	260	46	29.8	10	25			
8:50	280	48	30.0	200	47	29.8	9	27		260	48	29.8	220	44	29.8	10	25			
9:00	320	49	31.8	200	46	29.8	9	27		280	49	29.7	200	43	29.8	10	25			

TEST 2
6:15 PM

COLE

7:10

20805 - SURF

PM

23

E-tube Data Sheet

Houlton, Maine

Operator Brian/Lance

Date 7/9/1996

10
min

Time	Core Unit										Surface Unit				
	T/R Set #101					T/R Set #102 P.A. 550 AC					T/R Set #201				
	mA	Kv	Spk/min	mA	Kv	Spk/min	Quench Inlet	Quench Outlet			mA	Kv	Spk/min	Quench Inlet	Quench Outlet
8:00							8	28						9	24
8:10							8	28						9	24
8:20							8	28						9	24
8:30							8	28						9	24
8:40							7	28						9	25
8:50							8	29						9	25
9:00							8	28						9	24
9:10							8	28						9	24
9:20							8	28						9	24
9:30							9	28						9	24
9:40							8	28						9	24
9:50							8	28						9	24
10:00							8	28						9	24
10:10							8	28						9	24
10:20							8	28						9	24
10:30							8	28						9	24
10:40							8	28						9	24
10:50							8	28						9	24
11:00							8	28						9	24
11:10							8	28						9	24
11:20							8	28						9	24
11:30							8	28						9	24
11:40							8	28						9	24
11:50							8	28						9	24

E-tube Data Sheet

Houlton, Maine

Operator Brian/Leah

Date 7/9/1996

Time	Core Unit										Surface Unit				
	T/R Set #101					T/R Set #102 <i>Pressure</i>					T/R Set #201				
	mA	Kv	Spk/ min	mA	Kv	Spk/ min	Quench Inlet	Quench Outlet			mA	Kv	Spk/ min	Quench Inlet	Quench Outlet
12:00							8	28						9	24
12:10							8	28						9	24
12:20							8	28						9	24
12:30							8	28						9	24
12:40							8	28						9	24
12:50							8	28						9	24
1:00							8	28						9	24
1:10							8	28						9	24
1:20							8	28						9	24
1:30							8	28						9	24
1:40							8	28						9	24
1:50							8	28						9	24
2:00							8	28						9	24
2:10							8	28						9	24
2:20							8	28						9	24
2:30							8	28						9	24
2:40							8	28						9	24
2:50							8	28						9	24
3:00							8	28						9	24
3:10							8	28						9	24
3:20							8	28						9	24
3:30							8	28						9	24
3:40							8	28						9	24
3:50							8	28						9	24

230
5/10/96

E-tube Data Sheet Houlton, Maine

Operator Peter/Lance

Date 7/9/1996

Time	Core Unit										Surface Unit				
	T/R Set #101					T/R Set #102 P ₂₅					T/R Set #201				
	mA	Kv	Spk/ min	mA	Kv	Spk/ min	Quench Inlet	Quench Outlet			mA	Kv	Spk/ min	Quench Inlet	Quench Outlet
4:00							8	28						9	24
4:10							8	28						9	24
4:20							8	28						9	24
4:30							8	28						9	24
4:40							8	28						9	24
4:50							8	28						9	24
5:00							8	28						9	24
5:10							8	28						9	24
5:20							8	28						9	24
5:30							8	28						9	24
5:40							8	28						9	24
5:50							8	28						9	24
6:00							8	28						9	24
6:10							8	28						9	24
6:20							8	28						9	24
6:30							8	28						9	24
6:40							8	28						9	24
6:50							8	28						9	24
7:00							8	28						9	24
7:10							8	28						9	24
7:20							8	28						9	24
7:30							8	28						9	24
7:40							8	28						9	24
7:50							8	28						9	24

Operator Danny/bence

Date 7/9/1996

Time	Core Unit						Surface Unit						Flush Time
	T/R Set #101			T/R Set #102 Pressure			T/R Set #201			T/R Set #202 Pressure			
	mA	Kv	Spk/min	mA	Kv	Spk/min	mA	Kv	Spk/min	Quench Inlet	Quench Outlet		
8:00												24	
8:10										9	9	24	
8:20										9	9	24	
8:30										9	9	24	
8:40										9	9	24	
8:50										9	9	24	
9:00										9	9	24	
9:10										9	9	24	
9:20													

E-tube Data Sheet

Houlton, Maine

Operator B. L. L. / L. L. L.

Date 7 / 9 / 1996

10 min.

Time	Core Unit										Surface Unit				
	T/R Set #101					T/R Set #102 T e m p.					T/R Set #201				
	mA	Kv	Spk/min	mA	Kv	Spk/min	Quench Inlet	Quench Outlet			mA	Kv	Spk/min	Quench Inlet	Quench Outlet
8:00							227	164						222	148
8:10							227	167						222	143
8:20							229	168						222	148
8:30							229	165						222	147
8:40							231	162						201	113
8:50							232	163						221	134
9:00							232	162						220	141
9:10							232	161						220	140
9:20							232	162						220	141
9:30							231	164						221	144
9:40							231	162						221	147
9:50							230	163						222	148
10:00							230	164						222	147
10:10							230	165						222	146
10:20							231	165						221	147
10:30							230	166						222	148
10:40							229	167						222	148
10:50							230	167						222	150
11:00							230	168						223	148
11:10							230	167						223	149
11:20							231	169						223	147
11:30							230	165						223	148
11:40							230	167						222	150
11:50							230	166						222	150

E-tube Data Sheet Houlton, Maine

Operator Bison/Lance

Date 7/19 / 1996

Surface Unit															
Core Unit															
T/R Set #101															
T/R Set #102 Temp															
T/R Set #201															
T/R Set #202 Temp															
Time	mA	Kv	Spk/ min	mA	Kv	Spk/ min	mA	Kv	Spk/ min	mA	Kv	Spk/ min	Quench Inlet	Quench Outlet	Flush Time
12:00													232	148	
12:10													231	147	
12:20													231	148	
12:30													230	150	
12:40													230	148	
12:50													230	150	
1:00													232	150	
1:10													221	146	
1:20													221	147	
1:30													230	147	
1:40													202	108	
1:50													213	141	
2:00													217	142	
2:10													213	143	
2:20													216	142	
2:30													219	141	
2:40													220	149	
2:50													221	148	
3:00													221	147	
3:10													222	150	
3:20													222	150	
3:30													222	151	
3:40													222	152	
3:50													222	152	

210 X
310 X

E-tube Data Sheet

Houlton, Maine

Operator Brian Leve

Date 7/19/1996

Time	Core Unit										Surface Unit				
	T/R Set #101					T/R Set #102					T/R Set #202				
	mA	Kv	Spk/min	mA	Kv	Spk/min	Quench Inlet	Quench Outlet	Temp	mA	Kv	Spk/min	Quench Inlet	Quench Outlet	Temp
4:00							220	170					220	154	
4:10							229	169					223	153	
4:20							228	167					223	151	
4:30							229	168					219	149	
4:40							229	167					219	149	
4:50							229	166					219	148	
5:00							229	167					219	149	
5:10							229	167					219	146	
5:20							228	165					222	149	
5:30							228	168					223	153	
5:40							Power Bump						Power Bump		
5:50							229	166					224	147	
6:00							229	167					223	146	
6:10							230	171					223	147	
6:20							230	172					222	148	
6:30							230	173					223	149	
6:40							229	171					223	150	
6:50							230	169					224	151	
7:00							230	170					224	151	
7:10							230	170					223	150	
7:20							231	169					223	150	
7:30							230	169					223	151	
7:40							230	171					221	147	
7:50							230	171					222	148	

6:00
5:31
5:32

5:40
5:31
5:32

6:00
6:10
6:12

6:20
6:30
6:32

7:51
7:52
7:53

Date 7/9/1996

Operator Denny/Lance

[illegible]

E-TUBE LOGSHEET

L.P., HOULTON, MAINE

AM OPERATOR _____

PM OPERATOR SD

DATE 7/9/96

T/R Control Panel Readings						Zycom			Begin / End of Shift Reading		
Core Unit						Quench		Mesh Pad	Outlet Press in H2O	Flush Water Gal	Make up Water Gal
T/R Set # 101			T/R Set # 102			Inlet Temp	Outlet Temp				
Time	mA	Kv	Spk/m	mA	Kv	Spk/m					
7	280	45	15.0	150	40	14.9	205	205	29		
11	290	50									
3											
7											
11	290	50	29.9	260	45	29.7	228	170	8	28	
3	240	45	29.8	160	45	29.8	229	169	8	28	

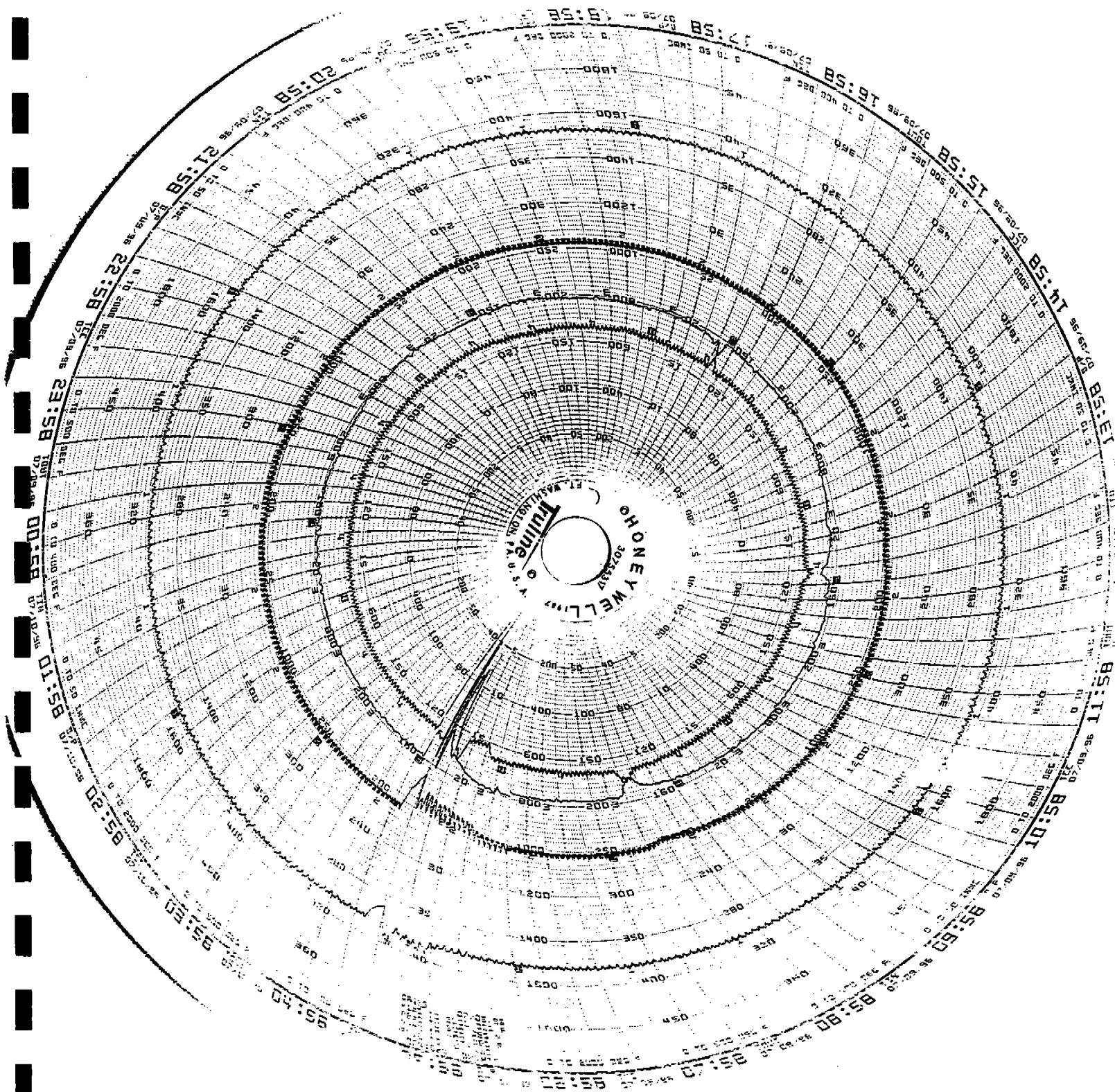
Surface Unit						Zycom			Begin / End of Shift Reading		
Core Unit						Quench		Mesh Pad	Outlet Press in H2O	Flush Water Gal	Make up Water Gal
T/R Set # 201			T/R Set # 202			Inlet Temp	Outlet Temp				
Time	mA	Kv	Spk/m	mA	Kv	Spk/m					
7	150	43	14.8	180	43	14.9	228	205	9	24	
11											
3											
7											
11	220	45	27.8	200	45	27.8	218	150	9	24	
3	220	45	29.9	220	45	29.7	220	149	9	24	

Sample Times:	
Recycle Water % Solids:	
pH	

Recycle Blowdown Gallons:	
---------------------------	--

Caustic	
End:	
Start:	
Total:	

Houlton Dryer RTO
7/9/96



RTO DATA SHEET HOULTON, MAINE

Operator Brent Carmichael

Press RTO

Dryer RTO X

Date 7/19/1996

RTO CHAMBER BEDS

Time	RTO CHAMBER BEDS							BURNERS			P-V					Δ				
	#1	#2	#3	#4	#5	#6	#7	Inlet Press	Burn #1	Burn #2	Burn #3	Inlet temp	Exh temp	Comb Temp	Press Drop	Gas meter				
10:00	369	344	392	405	393	361	385	1.1	1515	1518	1518	151	238	1521	16	650327				
10:10	368	343	397	405	391	363	387	0.9	1498	1505	1505	151	243	1523	15	650404				
10:20	369	346	393	402	394	363	385	1.0	1531	1516	1508	151	243	1521	15	650448				
10:30	369	344	398	406	392	364	388	1.0	1496	1504	1506	151	242	1526	15	650472				
10:40	369	346	394	402	395	364	386	1.0	1531	1517	1507	152	248	1529	16	650549				
10:50	368	344	399	403	392	365	388	1.1	1498	1511	1507	153	250	1520	15	650582				
11:00	368	344	399	404	392	365	388	1.0	1498	1507	1506	153	249	1524	15	650621				
11:10	369	345	399	403	393	365	388	1.0	1499	1511	1506	153	248	1523	15	650673				
11:20	370	347	394	403	395	365	388	1.0	1526	1518	1509	153	245	1526	16	650761				
11:30	370	346	399	402	393	366	388	1.1	1497	1511	1506	152	250	1523	15	650789				
11:40	371	347	393	405	396	364	388	1.1	1522	1519	1513	152	242	1526	15	650839				
11:50	371	345	399	405	393	365	390	0.9	1448	1504	1506	153	246	1524	16	650893				
12:00	370	347	394	403	396	364	388	0.9	1532	1518	1509	153	249	1530	15	650929				
12:10	370	345	399	404	393	365	390	0.9	1499	1504	1508	152	243	1531	15	650977				
12:20	370	345	398	406	393	365	390	1.0	1508	1516	1519	153	246	1531	16	651030				
12:30	370	346	399	402	394	366	389	1.0	1512	1509	1507	154	252	1520	16	651081				
12:40	371	346	397	407	394	364	391	0.9	1499	1501	1514	153	243	1520	15	651139				
12:50	371	348	395	402	396	365	388	1.0	1499	1513	1508	154	244	1524	15	651175				
1:00	372	347	393	406	397	364	390	0.9	1509	1514	1518	154	242	1517	16	651224				
1:10	370	348	398	401	396	366	389	1.0	1509	1510	1506	153	253	1520	16	651279				
1:20	372	347	395	409	396	363	390	1.0	1510	1512	1517	151	243	1515	15	651318				
1:30	369	347	398	401	395	365	389	1.0	1509	1506	1508	152	252	1518	16	651370				
1:40	371	346	395	409	394	362	390	1.0	1498	1498	1511	145	241	1516	16	651424				
1:50	369	346	397	400	394	364	388	0.9	1498	1507	1506	146	239	1515	16	651464				
2:00	368	344	397	403	392	362	388	0.9	1497	1507	1506	150	245	1524	15	651528				
2:10	368	346	395	400	394	362	386	1.1	1529	1514	1509	151	248	1529	16	651578				
2:20	370	344	394	407	393	361	389	1.0	1499	1504	1517	152	241	1512	16	651639				
2:30	370	345	392	405	395	361	388	1.1	1521	1516	1511	150	242	1521	16	651679				

AM

PM

W

RTO DATA SHEET

HOULTON, MAINE

Operator Brent Carmichael

Press RTO

Dryer RTO X

Date 7/19/1996

RTO CHAMBER BEDS										P-V			BURNERS			Inlet temp	Exh temp	Comb Temp	Press Drop	Gas meter
Time	#1	#2	#3	#4	#5	#6	#7	Inlet Press	Burn #1	Burn #2	Burn #3									
2:40	370	344	396	406	393	361	389	1.0	1499	1500	1511	152	241	1520	15	657285				
2:50	370	345	391	405	395	361	388	1.0	1521	1515	1512	152	243	1521	16	657289				
3:00	370	344	396	407	393	361	390	1.0	1500	1508	1515	153	242	1515	16	657283				
3:10	370	346	394	402	395	363	388	1.1	1529	1513	1508	153	250	1524	16	657282				
3:20	371	345	394	407	394	361	388	1.1	1515	1516	1515	154	243	1523	16	657285				
3:30	371	346	394	405	396	362	389	1.0	1526	1519	1511	155	246	1526	16	657281				
3:40	370	346	401	403	394	365	392	0.9	1497	1510	1507	157	250	1526	16	652088				
3:50	372	348	396	407	396	364	391	1.1	1522	1516	1511	155	246	1522	16	652042				
4:00	371	347	402	404	394	366	391	1.0	1508	1511	1509	156	254	1521	16	652049				
4:10	373	348	396	409	396	364	392	1.1	1518	1517	1514	155	243	1518	16	652047				
4:20	372	348	401	403	395	366	392	0.9	1498	1502	1507	155	244	1521	16	652047				
4:30	372	347	401	405	395	365	393	0.9	1497	1509	1506	154	250	1527	16	652042				
4:40	371	348	399	401	396	366	391	1.0	1512	1511	1507	154	252	1522	16	652042				
4:50	373	349	399	409	394	364	393	0.9	1501	1502	1515	153	243	1513	16	652047				
5:00	371	348	399	401	395	365	391	1.0	1504	1513	1508	153	254	1523	16	652047				
5:10	372	348	395	405	396	364	390	1.0	1521	1511	1509	153	254	1525	16	652046				
5:20	372	347	398	408	395	363	392	1.0	1511	1513	1513	153	248	1527	16	652046				
5:30	373	348	394	405	397	363	390	1.1	1523	1520	1507	155	254	1522	16	652047				
5:40	371	349	397	401	396	365	390	.9	1499	1509	1507	143	249	1524	17	652049				
5:50	370	348	399	400	395	366	391	.8	1497	1505	1505	157	243	1511	16	652047				
6:00	370	347	397	406	395	364	389	.9	1499	1502	1513	152	246	1514	16	652047				
6:10	371	349	398	401	394	363	391	.1	1499	1501	1511	157	241	1521	16	652047				
6:20	370	348	399	400	395	365	390	.7	1501	1505	1515	154	242	1521	16	652047				
6:30	371	348	396	402	395	365	389	1.0	1507	1506	1508	155	252	1514	16	652046				
6:40	371	345	395	403	396	364	390	1.0	1510	1508	1505	154	251	1520	16	652046				
6:50	373	348	396	406	396	365	391	1.0	1523	1510	1508	155	254	1521	16	652047				
7:00	371	348	400	401	395	367	391	1.0	1496	1509	1507	155	248	1523	16	652047				
7:10	373	347	399	407	395	365	393	1.0	1530	1517	1507	154	251	1523	16	652047				

PM

WS

205-222-4413

Operator Brent Carmichael

Press RTO

Dryer RTO

X

Date _____

7, 9 1996

[illegible]

RTO LOGSHEET

Press _____

HOULTON, MAINE

Dryer ☒

AM OPERATOR J. CHARETTE PM OPERATOR S.D. DATE 7 / 9 / 96

BURNER #1 SETPOINT
BURNER #1 TEMP
BURNER #1 OUTPUT
BURNER #2 SETPOINT
BURNER #2 TEMP
BURNER #2 OUTPUT
BURNER #3 SETPOINT
BURNER #3 TEMP
BURNER #3 OUTPUT
INLET TEMP
CHAMBER TEMP
EXHAUST TEMP
INLET PRESS
DELTA PRESS
VFD #1 AMPS
VFD #1 RPM
VFD #2 AMPS
VFD #2 RPM
P/V SETPOINT
P/V OUTPUT
RECOV CH 1 TEMP
RECOV CH 2 TEMP
RECOV CH 3 TEMP
RECOV CH 4 TEMP
RECOV CH 5 TEMP
RECOV CH 6 TEMP
RECOV CH 7 TEMP
FAN #1 SHAFT BRG
FAN #1 FAN BRG
FAN #2 SHAFT BRG
FAN #2 FAN BRG
PURGE FAN RUNNING
BTUE SYSTEM ON
RTO GAS INLET PRESS

VAPORIZ WATER TEMP
VAPORIZ INLET PRESS
VAPORIZ OUTLET PRE

GAS METER READING

[illegible]

RTO OPERATOR'S LOG #1

HOULTON, ME.

Date: 7-9-96

Shift Electrician inspect the RTO outside and take the following readings every two hours. Press Lineman to fill in when Electrician is busy.

DataLiner:

Recovery Chamber Temperatures					Inlet Press. W.C.	Inlet Temp	Comb. Chamber Temp.	Exh. Temp.
1	2	3	4	5				
341	328	343	350	342	4.4	123	1537	237
346	332	345	355	343	4.3	126	1549	238
348	337	346	361	344	4.2	128	1550	241
348	333	353	347	349	4.3	128	1552	239
344	336	346	352	351	4.4	126	1548	235
348	334	346	350	350	4.1	125	1524	231

Shift (at 12 AM): Propane tank #1 72 % Tank #2 64 %

Log startup/shutdown times, problems, maintenance items, etc.:
(use chartrecorder time)

RTO OPERATOR'S LOG #2

HOULTON, ME.

Date:

7-9-96

Shift Electrician inspect the RTO outside and take the following readings every FOUR hours. Press Lineman to fill in when Electrician is busy. Propane readings: 3 X per shift, Vaporizer: 1 X per shift.

RTO Delta P	Press. Inlet Duct	Burner		Motor Amps	Propane		Temperature Vaporizer
		Temperature #1	Output % #2		Pressures RTO	Vaporizer In Out	

M	17	4.5	1549	1552	9.0	1.1	113	7	90	8	135
2	18	4.3	1544	1552	2.0	0	108				
3	18	4.1	1532	1545	14.0	0	113				
M	17	4.3	1529	1531	42.2	54.6	111	7	120	8	134
1	17	4.2	1549	1554	0.4	2.2	111				
3	17	4.1	1528	1533	34.6	0.4	111				

Burner Setpoints: 1) 1535

BTUE SYSTEM: ON

OFF

2) 1535

Readings taken by: DAY

S. Traw

NITE

S. D.

HOULTON BOARD WEIGHTS

(lbs./8x16 panel every 25th mat during test Times)

APPROXIMATE TIMES

7/16"

07/09/96

KG	LBS
90.80	200.21
90.60	199.77
79.10	174.42
92.10	203.08
92.40	203.74
85.90	189.41
90.50	199.55
93.00	205.07
94.10	207.49
91.30	201.32
89.00	196.25
89.00	196.25
88.10	194.26
88.90	196.02
91.60	201.98
91.60	201.98
90.40	199.33
87.20	192.28
88.60	195.36
86.50	190.73
89.60	197.57
88.90	196.02
89.40	197.13
89.90	198.23
89.70	197.79
90.30	199.11
86.80	191.39
93.30	205.73
89.50	197.35
93.60	206.39
92.70	204.40
93.10	205.29
91.10	200.88
92.40	203.74
93.80	206.83
100.10	220.72
96.90	213.66
95.60	210.80
96.40	212.56
95.00	209.48
93.70	206.61
98.00	216.09
94.80	209.03
95.60	210.80
92.80	204.62
91.90	202.64
92.80	204.62
90.20	198.89
91.30	201.32
	201.5955

7% TRIM
8x16 WT.
4x8 NET

187.48
46.87

07/10/96

KG	LBS
85.70	188.97
90.70	199.99
90.10	198.67
89.30	196.91
88.10	194.26
89.10	196.47
90.60	199.77
92.90	204.84
88.60	195.36
89.50	197.35
92.90	204.84
92.50	203.96
90.60	199.77
90.10	198.67
90.30	199.11
91.70	202.20
90.30	199.11
90.90	200.43
93.10	205.29
94.10	207.49
91.10	200.88
93.20	205.51
93.10	205.29
93.00	205.07
93.50	206.17
93.70	206.61
91.80	202.42
94.40	208.15
93.50	206.17
93.20	205.51
88.40	194.92
90.30	199.11
90.00	198.45
89.80	198.01
92.20	203.30
89.90	198.23
92.10	203.08
92.90	204.84
93.50	206.17
90.20	198.89
91.30	201.32
94.10	207.49
94.30	207.93
92.30	203.52
91.60	201.98
	0.00
	0.00
	0.00
	0.00
	201.6105

7% TRIM
8x16 WT.
4x8 NET

187.50
46.87

AIR POLLUTION SOURCE and CONTROL EQUIPMENT LOGSHEET

Operator DAN H. Crew D AM PM Date 7/9/96

Log the start/stop, (open/shut) times of the following Sources & Control Equipment. Use the time displayed on the telephone.

Sources: Forming Line, Dryers, Thermal Oil Heaters, RTO's,
RTO Bypass Stack Damper (open/shut).

Control Equipment: ESP's, E-tubes, RTO's (Press/Dryer), &
Baghouses

<u>Time</u>	<u>Item</u>	<u>Operation</u>	<u>Comment</u>
5:40 ^{AM}	Lost ALL Power	Stop	Everything Down
5:44 ^{AM}	#2 E.S.P. + #2 Korus	Start	Power is back
5:46 ^{AM}	Baghouse	Start	" " "
5:50 ^{AM}	E-Tubes (Both)	Start	" " "
5:56 ^{AM}	R.T.O.	Start	" " "
5:56 ^{AM}	Both dryers	Start	" " "

Use Reverse side for additional space.

FORMS/s-log

AIR POLLUTION SOURCE and CONTROL EQUIPMENT LOGSHEET

Operator Brian Crew A (AM) PM Date 7-9-96

Log the start/stop, (open/shut) times of the following Sources & Control Equipment. Use the time displayed on the telephone.

Sources: Forming Line, Dryers, Thermal Oil Heaters, RTO's,
RTO Bypass Stack Damper (open/shut).

Control Equipment: ESP's, E-tubes, RTO's (Press/Dryer), &
Baghouses

<u>Time</u>	<u>Item</u>	<u>Operation</u>	<u>Comment</u>
847	SL dryer	STOP	Dry bin Full
857	SL dryer	Start	
140	SL dryer	stop	Wood Fuel Flame went out
143	SL dryer	Start	Started on oil, wood Nugs
540	SL + CL dryer	stop	Power Bump
542	SL + CL dryer	start	

Use Reverse side for additional space.

FORMS/s-log

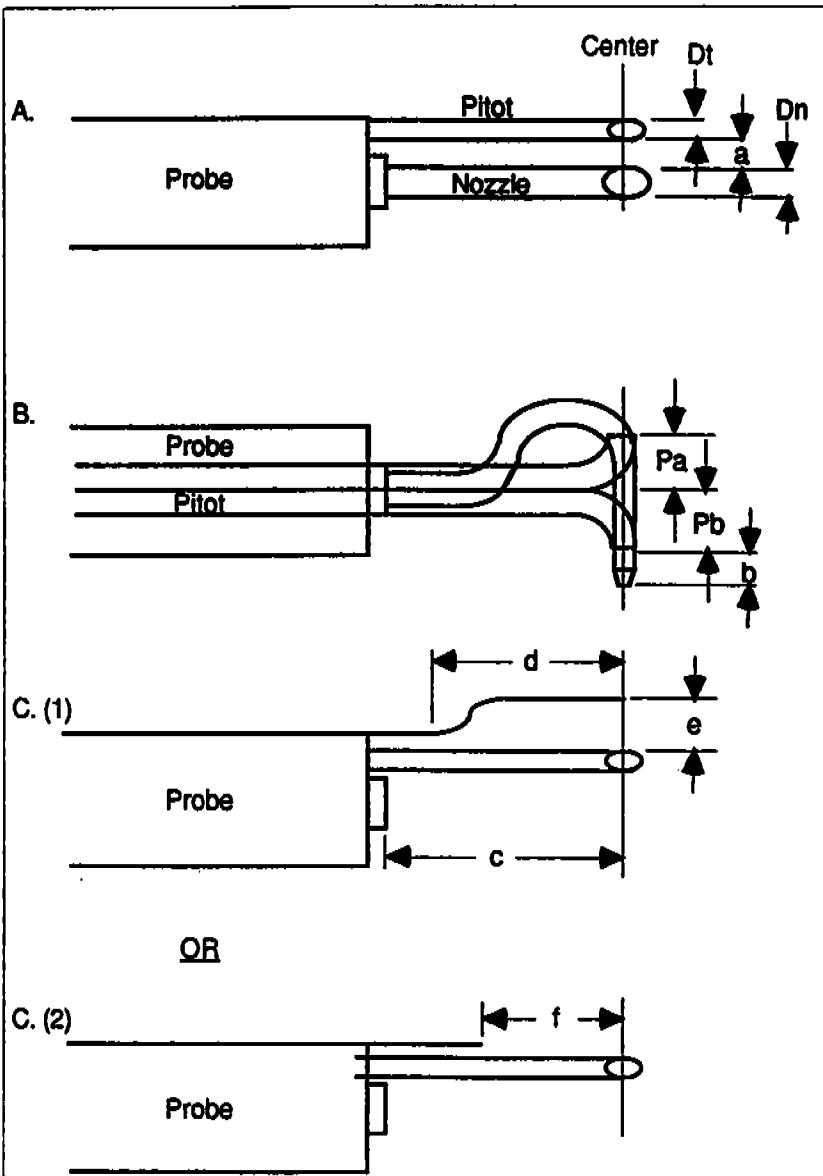
APPENDIX F
Equipment Calibration
&
CEMS Gas Certifications

Probe Identification 401

Pitot Identification 401

Technical Specialist EMOST

Date 4/26/96



Dt 0.374
Dn 0.500
a 0.785

Pa 0.567
Pb 0.567
b 1.067

c 5.073
d 4.502
e 0.792

OR

OR

c _____
f _____

Specifications (EPA Method 2)

Dt = 3/16" to 3/8"

Dn = 1/2"

a ≥ 3/4"

b ≥ 0

c ≥ 3"

d ≥ 3"

e ≥ 3/4"

f ≥ 2"

Pa = Pb

1.05 Dt ≤ P ≤ 1.50 Dt

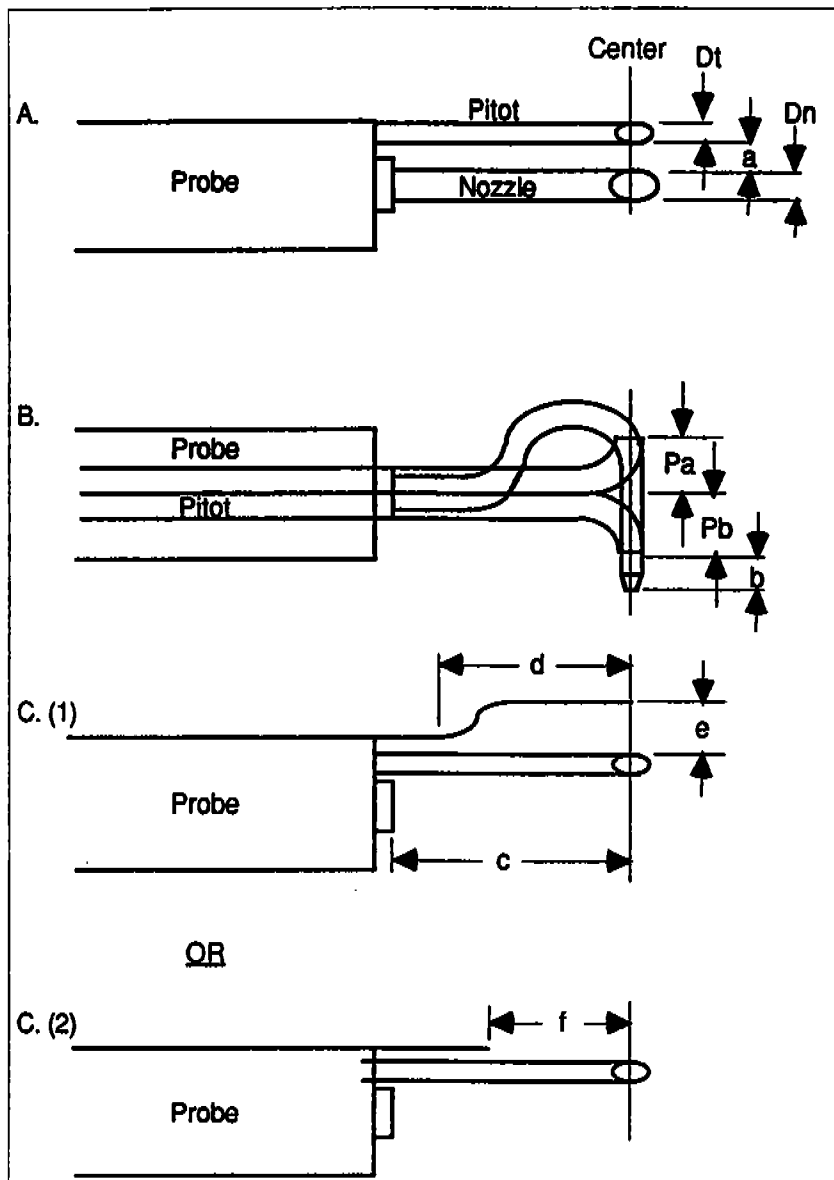
If these specifications are met, proceed with Part 2, Pitot alignment.

Probe Identification 601

Pitot Identification 601

Technical Specialist EMOST

Date 4/26/96



Dt 0.374

Dn 0.622

a 0.753

Pa 0.517

Pb 0.517

b 0.923

c 5.312

d 3.360

e 0.782

OR

OR

c _____

f _____

Specifications (EPA Method 2)

Dt = 3/16" to 3/8"

Dn = 1/2"

a ≥ 3/4"

b ≥ 0

c ≥ 3"

d ≥ 3"

e ≥ 3/4"

f ≥ 2"

Pa = Pb

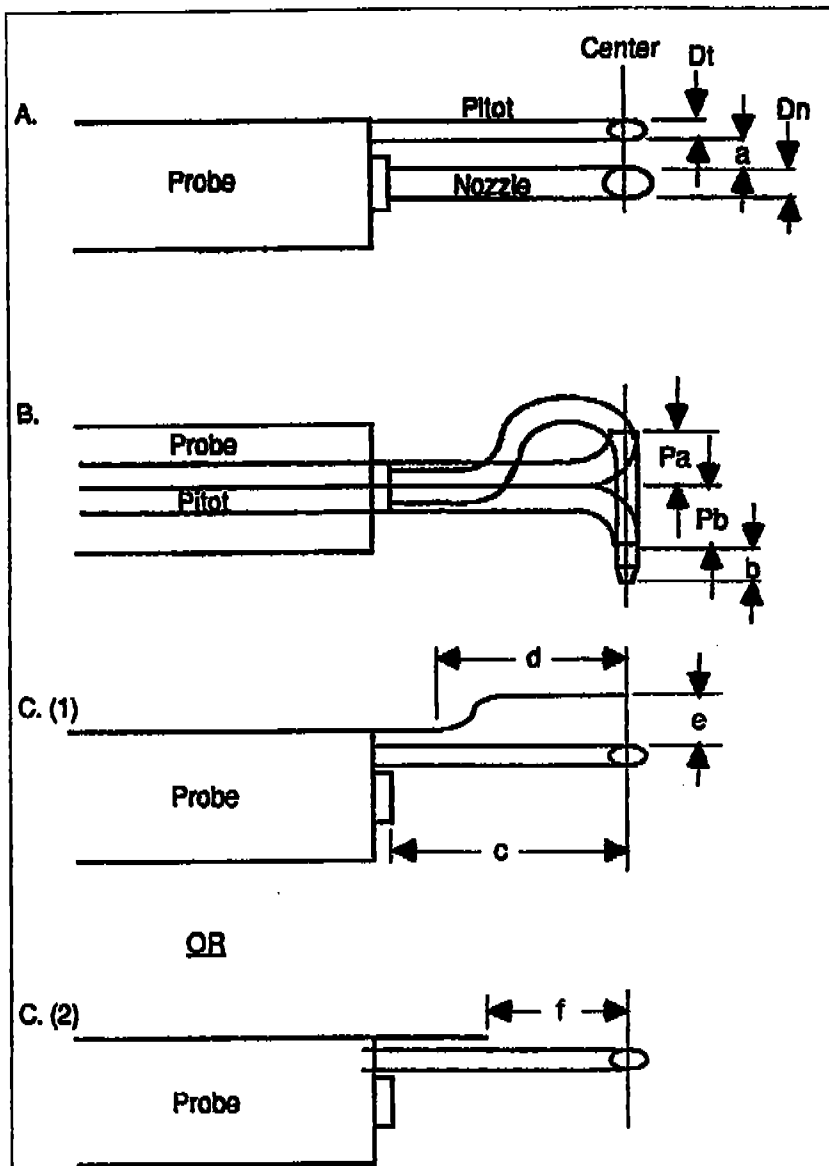
1.05 Dt ≤ P ≤ 1.50 Dt

If these specifications are met, proceed with Part 2, Pitot alignment.



S-Type Pitot Tube Geometric Calibration Part 1 - Probe Configuration

Probe Identification 902 Pitot Identification 902
 Technical Specialist EMOST
 Date 4/26/96



Dt 0.0378
 Dn 0.625
 a 0.778

Pa 0.515
 Pb 0.515
 b 0.778

c 5.897
 d 4.375
 e 1.059

OR

OR

c _____
 f _____

Specifications (EPA Method 2)

Dt = 3/16" to 3/8"
 Dn = 1/2"
 a ≥ 3/4"
 b ≥ 0

c ≥ 3"
 d ≥ 3"
 e ≥ 3/4"
 f ≥ 2"

Pa = Pb

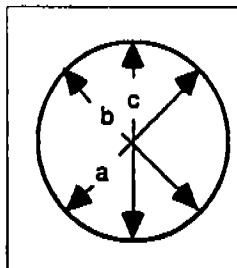
1.05 Dt ≤ P ≤ 1.50 Dt

If these specifications are met, proceed with Part 2, Pitot alignment.

Nozzle Set Number #1

Tech Specialist E. MOST

Date Calibrated 4/11/96



Nozzle Number	Diameter*	a	b	c	Average**
1-1	3/16	0.177	0.178	0.178	0.178
1-2	1/4	0.252	0.253	0.252	0.252
1-3	9/32	0.276	0.274	0.274	0.275
1-4	3/8	0.374	0.373	0.375	0.374
1-5	13/32	0.406	0.406	0.407	0.406
1-6	1/2	0.492	0.493	0.493	0.493
1-7	5/16	0.313	0.314	0.314	0.314
1-8	7/32	0.208	0.208	0.209	0.208

*NOTE: Measure to the nearest 0.001".

**NOTE: The three measurements must be within 0.004" of each other.

CRITICAL ORIFICE METHOD 5 MODULE CALIBRATION

PUMP NUMBER: 3

MODULE NUMBER: 98

NAME: E. MOST

BAROMETRIC PRESSURE: 29.60

DATE: 4/8/96

STANDARD METER DGM-115

PRE-CAL

POST-CAL FROM

MODULE			ORIFICE		MODULE METER										CALIBRATIONS		
PUMP VACUUM* (in. Hg)	ΔH SETTING (in. H ₂ O)	TEMP. T _{amb} (°F)	NUMBER	K'	VOLUME V _{ml} (cubic ft.)	VOLUME V _{mf} (cubic ft.)	VOLUME V _m (cubic ft.)	TEMP. T _{mi} (°F)	TEMP. T _{mf} (°F)	TEMP. T _m (°F)	TIME ∞ (min)	V _m (std)	V _{cr} (std)	Y	Variability	ΔH@	
15	0.62	67	AC47	0.3146	501.27	503.39	2.12	66	66	66	5.00	2.11	2.03	0.96	-0.04	2.11	
15	1.20	66	AC 55	0.4378	503.63	506.47	2.84	66	66	66	5.00	2.83	2.83	1.00	0.00	2.11	
15	1.90	65	AC 63	0.5633	506.67	510.30	3.63	68	66	67	5.00	3.61	3.64	1.01	0.01	2.02	
15	3.50	64	AC 73	0.7647	510.76	515.71	4.95	70	67	69	5.00	4.93	4.94	1.00	0.00	2.02	
15	4.90	64	AC 81	0.9468	516.07	522.07	6.00	72	67	70	5.00	5.99	6.12	1.02	0.02	1.86	
														1.00	0.00	2.03	

***NOTE:** Each orifice has a pre-calibrated critical vacuum of 14" Hg, set module vacuum at 1" to 2" above critical vacuum.

*NOTE: Each orifice has a pre-calibrated critical vacuum of 14" Hg, set module vacuum at 1" to 2" above critical vacuum.

$$Vcr(std) = \frac{K Pbar_{\infty}}{\sqrt{T_{amb}}}$$

$$Vm(std) = 17.64 Vm \frac{(Pbar + \Delta H/13.6)}{(Tm + 460)}$$

$$Y = \frac{Vcr(std)}{Vm(std)}$$

$$\Delta H@ = 0.0319 \Delta H \frac{(Tm + 460)}{Pbar (Y Vm)^{0.2}}$$

Module Leak Check: X
 Pilot Leak Check: X
 Probe Heat Control: X
 Heater Box Control: X
 T.C. Readout calibrated with: Hot / Cold Bath
 Constant Voltage Source

**** CERTIFICATE OF ANALYSIS - EPA PROTOCOL MIXTURE ****

CUSTOMER: ABCO WELDING & INDUSTRIAL SUPPLY
CYLINDER #: SX-37453
CYLINDER PRESSURE: 2,000 psig
LAST ANALYSIS DATE: 04-05-96
EXPIRATION DATE: 04-05-99

REFERENCE #: 109-48682
PROTOCOL: 1

DO NOT USE THIS CYLINDER WHEN THE
PRESSURE FALLS BELOW 150 psig

Component: CARBON DIOXIDE

REPLICATE CONCENTRATIONS

Date: 04-05-96

12.6 PCT

12.6 PCT

12.6 PCT

Mean Conc: 12.6 PCT

COMPONENT: OXYGEN

Date: 04-05-96

Date:

12.8 PCT

12.8 PCT

12.8 PCT

Mean Conc: 12.8 PCT

BALANCE GAS: NITROGEN

REFERENCE STANDARDS

SRM #: 1674B

GMIS2659G

CYLINDER #: CLM-6492

SX-30352

CONCENTRATION: 6.98 PCT

20.34 PCT

CERTIFICATION INSTRUMENTS

COMPONENT CARBON DIOXIDE

MAKE/MODEL Horiba VIA 510

SERIAL NUMBER 850802052

MEASUREMENT PRINC. NDIR

LAST CALIBRATION 03-19-96

OXYGEN

Rosemount 755

2002832

Paramagnetic

04-01-96

THIS CERTIFICATION WAS PERFORMED ACCORDING TO EPA TRACEABILITY PROTOCOL FOR
ASSAY & CERTIFICATION OF GASEOUS CALIBRATION STANDARDS REVISED SEPT. 1993,
USING PROCEDURE G1 AND/OR G2. THE TOTAL ANALYTICAL UNCERTAINTY OF THIS
MIXTURE IS ESTIMATED TO BE ± OR - 1%.

ANALYST

Thomas J. Purdon

DATE

4/10/96

**** CERTIFICATE OF ANALYSIS - EPA PROTOCOL MIXTURE ****

CUSTOMER: ABCO WELDING & INDUSTRIAL SUPPLY
CYLINDER #: SX-37445
CYLINDER PRESSURE: 2,000 psig
LAST ANALYSIS DATE: 04-05-96
EXPIRATION DATE: 04-05-99

REFERENCE #: 109-48682
PROTOCOL: 1

DO NOT USE THIS CYLINDER WHEN THE
PRESSURE FALLS BELOW 150 psig

Component: CARBON DIOXIDE

REPLICATE CONCENTRATIONS
Date: 04-05-96

Mean Conc: 19.7 PCT

19.7 PCT
19.7 PCT
19.6 PCT

COMPONENT: OXYGEN

Date: 04-05-96

Date:

Mean Conc: 22.6 PCT

22.6 PCT
22.6 PCT
22.6 PCT

BALANCE GAS: NITROGEN

REFERENCE STANDARDS

SRM #: 1674B
CYLINDER #: CLM-6492
CONCENTRATION: 6.98 PCT

GMIS2659G
SX-30352
20.34 PCT

CERTIFICATION INSTRUMENTS

COMPONENT	CARBON DIOXIDE
MAKE/MODEL	Horiba VIA 510
SERIAL NUMBER	850802052
MEASUREMENT PRINC.	NDIR
LAST CALIBRATION	03-19-96

OXYGEN
Rosemount 755
2002832
Paramagnetic
04-01-96

THIS CERTIFICATION WAS PERFORMED ACCORDING TO EPA TRACEABILITY PROTOCOL FOR
ASSAY & CERTIFICATION OF GASEOUS CALIBRATION STANDARDS REVISED SEPT. 1993,
USING PROCEDURE G1 AND/OR G2. THE TOTAL ANALYTICAL UNCERTAINTY OF THIS
MIXTURE IS ESTIMATED TO BE + OR - 1%.

ANALYST

Thomas J. Pardon

DATE

4/15/96

Scott Specialty Gases, Inc.

2330 HAMILTON BOULEVARD
SOUTH PLAINFIELD NJ 07080
Phone: 908-754-7700

FAX: 908-754-7303

CERTIFICATE OF ANALYSIS

AIR POLLUTION CHARACTER
EARL MOST
AND CONTROL
60 INDUSTRIAL PK RD WEST
TOLLAND

CT 06084

PROJECT #: 07-24580-004
POM: C41389
ITEM #: 07022751 4AL
DATE: 12/16/93

CYLINDER #: AL4008186

ANALYTICAL ACCURACY: $\pm 2\%$

BLENDED TYPE: CERTIFIED MASTER GAS

COMPONENT
METHANE
NITROGEN

REQUESTED GAS
CONC. MOLES
275. PPM
BAL

ANALYSIS
(MOLES)
282. PPM
BAL

CERTIFIED

ANALYST

JOHN O'SHEA

PLUMSTEADVILLE, PENNSYLVANIA / TROY, MICHIGAN / HOUSTON, TEXAS / DURHAM, NORTH CAROLINA
SOUTH PLAINFIELD, NEW JERSEY / FREMONT, CALIFORNIA / WAKEFIELD, MASSACHUSETTS / LONGMONT, COLORADO
BATON ROUGE, LOUISIANA

Scott Specialty Gases, Inc.

RECEIVED JUL 2 - 1993

Shipped 2330 HAMILTON BOULEVARD
From: SOUTH PLAINFIELD NJ 07080
Phone: 908-754-7700

Fax: 908-754-7303

C E R T I F I C A T E O F A N A L Y S I S

ATR POLLUTION CHARACTER
EARL MOST
AND CONTROL
60 INDUSTRIAL PK RD WEST
TOLLAND

CT 06084

PROJECT #: 07-21664-001
PO#: 1194 EM
ITEM #: 07022751 4AL
DATE: 6/24/93

~~CYLINDER # 1-AL-06084-15~~

ANALYTICAL ACCURACY: \pm 2 %

BLEND TYPE : CERTIFIED MASTER GAS

COMPONENT
METHANE
NITROGEN

REQUESTED GAS
--CONC MOLES--
500. PPM
BAL

ANALYSIS
(MOLES)
~~500. PPM~~
BAL

ANALYST: 271

JOHN O'SHEA

APPROVED BY: [Signature]

ADELA SY

GREAT LAKES AIRGAS INC

***** CERTIFICATE OF ANALYSIS *****

Customer: Connecticut Airgas

June 21 1995

Test Report GM 48195

PRIMARY STANDARD GRADE

CYLINDER NUMBER	REQUESTED COMPOSITION		REPORTED COMPOSITION	
CC26728	900ppm Balance	Methane Nitrogen	911ppm Balance	Methane Nitrogen
CC97937	900ppm Balance	Methane Nitrogen	901ppm Balance	Methane Nitrogen


Approved for Release

ANALYTICAL REPORT

Form Reported: 10-1-84
Form Order No: 35-38-32-1-84
Purchase Order: 35-38-32-1-84

at Connecticut Gasgas/Presto Div
441 Garkett Point Road
North Haven, CT 06473
203-288-8381

Order No: 33879
Item Ordered: 100 ppm Methane/Nitrogen Primary Standard

Order No:	Component	Specification	Concentration
[REDACTED]	Methane Nitrogen	100 ppm Balance	[REDACTED] Balance

Method of Analysis: Gas Chromatography
Gas Chromatography

Previous Analysis:

CRYODYNE Gas Analyst

This report states good use of the results of the investigation made upon materials submitted to the analytical laboratory. Every effort has been made to determine objectively the information requested. However, in connection with its rendering of this report, CRYODYNE TECHNOLOGIES, INC., shall have no liability in excess of its established charge for the service. Any use of this report or the information contained herein shall be at the sole risk of the user.

NATIONAL SPECIALTY GASES
630 UNITED DRIVE
DURHAM, NC 27713
(919)544-3772

CERTIFICATE OF ANALYSIS-EPA PROTOCOL MIXTURES

REFERENCE #: 89-37794
CYL. PRESSURE: 2000PSIG
ANALYSIS DATE: 2/1/95
CUSTOMER: CONNECTICUT AIRGAS P.O.# 15645

METHOD: ANALYZED ACCORDING TO EPA TRACEABILITY PROTOCOL FOR ASSAY AND CERTIFICATION
OF GASEOUS CALIBRATION STANDARDS-SEPTEMBER 1993:G-1

STANDARD:
SRM #: 1659A
CYL #: CLM3081
CONC.: 9.65PPM

INSTRUMENT: BECKMAN THC
MODEL #: 400
SERIAL #: 1003052
LAST CAL.: 1/10/95

COMPONENT: CH
REPLICATE CONC.
DATE: 2/1/95 DATE:
16.2PPM
16.3PPM
16.3PPM

COMPONENT:
MEAN CONC:
REPLICATE CONC.
DATE: DATE:

COMPONENT:
MEAN CONC:
REPLICATE CONC.
DATE: DATE:

BALANCE GAS: N2

REPLICATE DATA

DATE: 2/1/95

Z	0	R	348.0	C	584.2
R	348.1	Z	0	C	588.0
Z	0	C	588.2	R	348.2

COMPONENT: CH4

DATE:

Z	R	C
R	Z	C
Z	C	R

REPLICATE DATA

DATE:

Z	R	C
R	Z	C
Z	C	R

COMPONENT:

DATE:

Z	R	C
R	Z	C
Z	C	R

REPLICATE DATA

DATE:

Z	R	C
R	Z	C
Z	C	R

COMPONENT:

DATE:

Z	R	C
R	Z	C
Z	C	R

Z=ZERO C=CANDIDATE R=REFERENCE

ANALYST: *Gray A. Savoy*

APPROVED BY: *John Hone*

"THIS REPORT STATED ACCURATELY THE RESULTS OF THE INVESTIGATION MADE UPON THE MATERIAL SUBMITTED TO THE ANALYTICAL LABORATORY. EVERY EFFORT HAS BEEN MADE TO DETERMINE OBJECTIVELY, THE INFORMATION REQUESTED; HOWEVER, IN CONNECTION WITH ITS RENDERING OF THIS REPORT, NATIONAL SPECIALTY GASES SHALL HAVE NO LIABILITY IN EXCESS OF ITS ESTABLISHED CHARGE FOR THE SERVICE."

GREAT LAKES AIRGAS INC

***** CERTIFICATE OF ANALYSIS *****

Customer: Connecticut Airgas

May 18 1995

Test Report GM 35895

PRIMARY MIXTURE

CYLINDER NUMBER	REQUESTED COMPOSITION	REPORTED COMPOSITION
65-110	50ppm Methane Balance Nitrogen	65-110 50ppm Methane Balance Nitrogen
65-110	50ppm Methane Balance Nitrogen	65-110 50ppm Methane Balance Nitrogen

Post-It Fax Note 7571		Date 6-9	Page 1
To	PETER	From	RAY
Co. Dept	APCC	Co.	AIRGAS
Phone #		Phone #	
Fax #	871-8625	Fax #	

INV. 72805

Ed Johnson
Approved for Release

GREAT LAKES AIRGAS INC

***** CERTIFICATE OF ANALYSIS *****

Customer: Connecticut Airgas

May 13 1995

Test Report GM 35995

PRIMARY MIXTURE

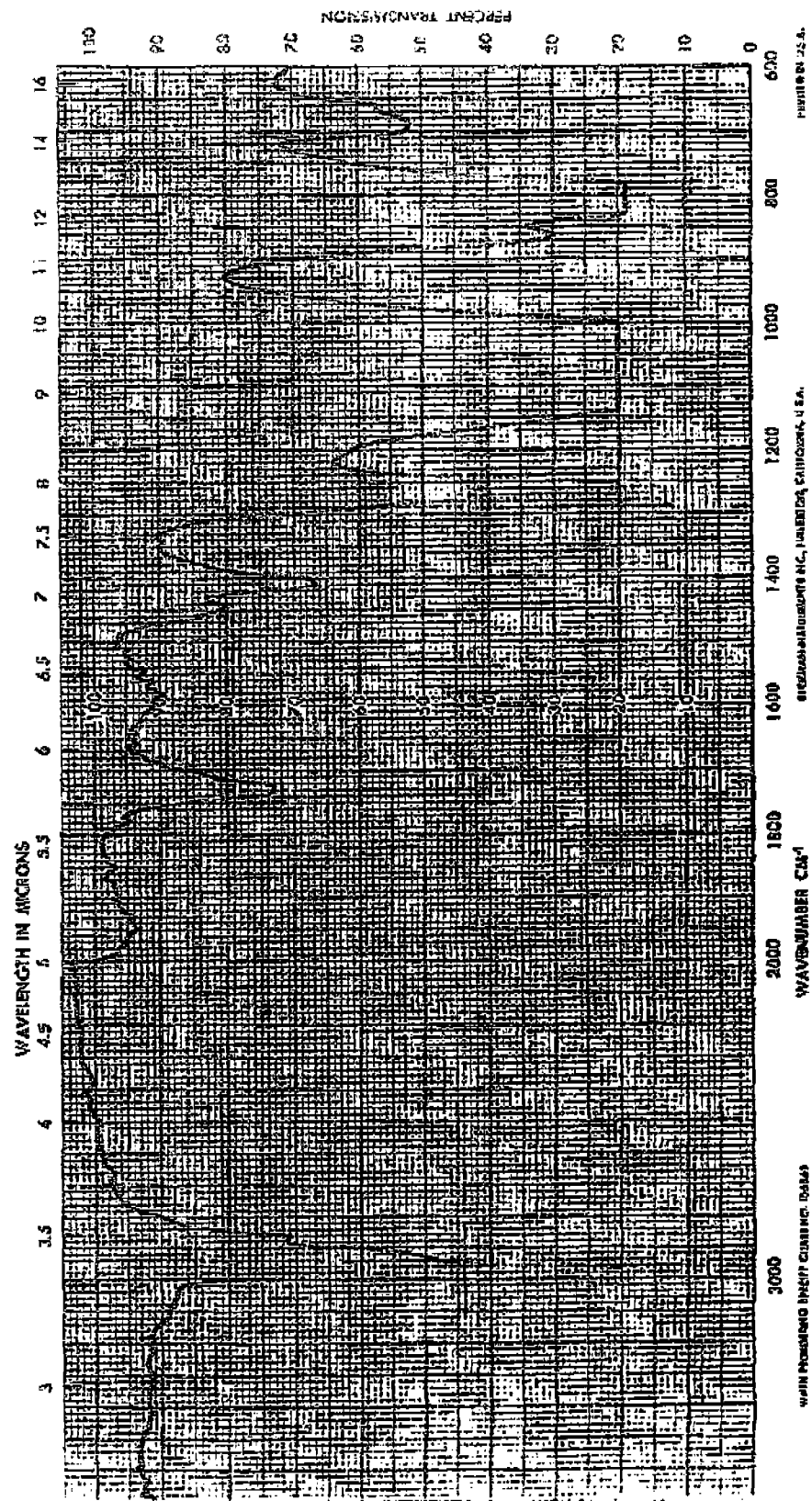
CYLINDER NUMBER	REQUESTED COMPOSITION	REPORTED COMPOSITION
[REDACTED]	35ppm Methane Balance Nitrogen	[REDACTED] Methane Balance Nitrogen
[REDACTED]	35ppm Methane Balance Nitrogen	[REDACTED] Methane Balance Nitrogen

Ed Johnson
Approved for Release

APPENDIX G
Laboratory Data

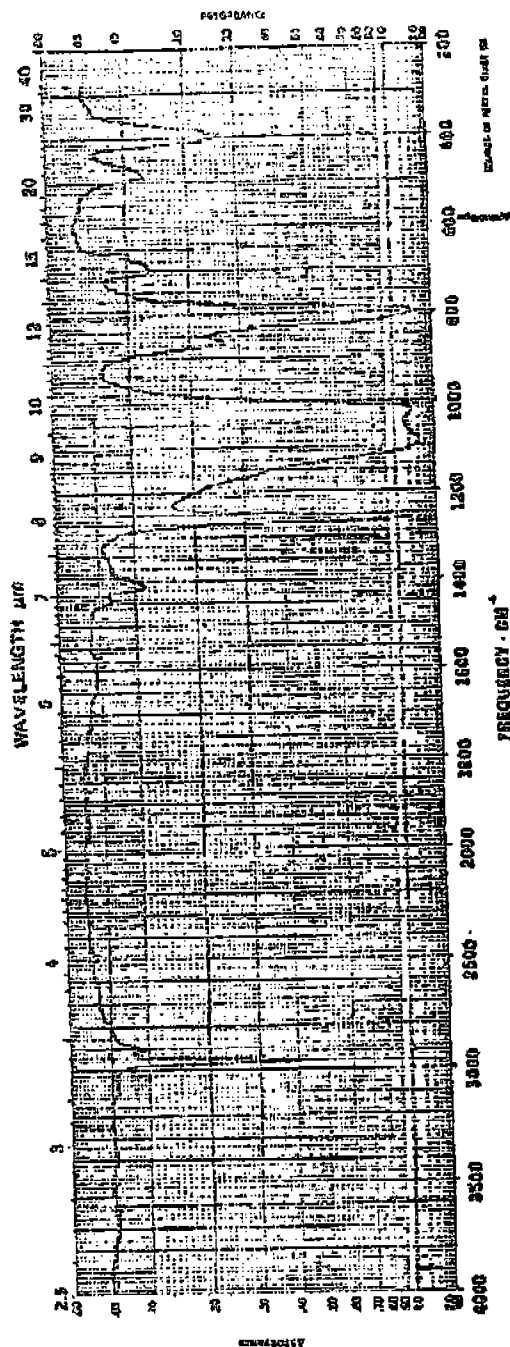
Thin film IR scan

Test 4/Run 1 organic

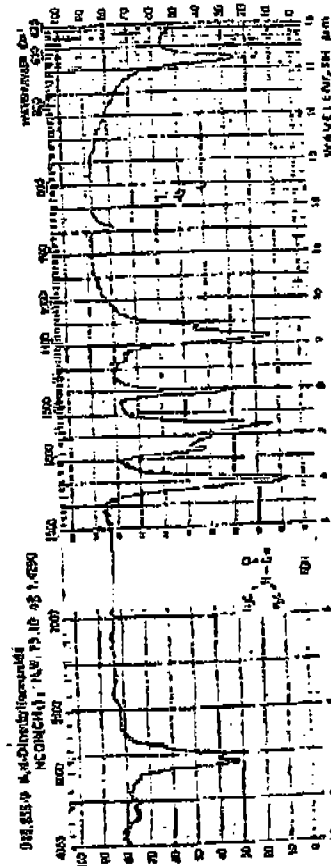


Source: Dow Corning Corp.,
Capillary Cell

SILICONE LUBRICANT



009 01 64993
was 1977





INTERPOLL LABORATORIES, INC.
4500 BALL ROAD N.E.
CIRCLE PINES, MINNESOTA 55014-1819
TEL: 612/786-6020
FAX: 612/786-7854

August 30, 1996

Sue Somers
Louisiana-Pacific Corporation
Northern Division
Rt. 8, Box 8263
Hayward, Wisconsin 54843

Dear Sue:

Interpoll Laboratories, Inc. received six (6) samples representing the organic and inorganic EPA Method 202 samples from Test 4, Runs 1-3. These samples were collected from the Dryer RTO Stack at the Louisiana-Pacific facility located in Houlton, Maine. The reason these samples were submitted to Interpoll Labs was the high organic fraction determined for Run 1 which appeared to be an outlier. The organic fraction of Run 1 was therefore resolubilized in methylene chloride and a thin film applied to a sodium chloride plate for infrared analysis. This technique was chosen as it is a nondestructive technique which would provide additional information as to the composition of the material. The instrument used in this work is a Beckman Microlab 600 Computing IR Spectrophotometer. The result of this IR scan is provided on the attachment. A tentative identification of this material was silicone grease, a common glass joint sealant used by most stack testing firms, however, use of this sealant is not recommended when performing EPA Method 202 as the methylene chloride does extract this compound from glass surfaces. A sample of Dow Corning silicone grease was therefore also run to provide a reference spectra, the result of that IR scan is shown below the sample run. A comparison of these two spectra indicate that the Test 4 Run 1 organic fraction does contain silicone grease. Note that this technique is not quantitative, therefore the exact amount of silicone grease cannot be determined, however, the "purity" of the spectra indicate that the sample contained a substantial quantity of silicone grease. Note that the other two organic fractions (Runs 2 & 3) were analyzed and found to contain silicone grease also.

Should you have any questions please do not hesitate to call me.

Sincerely,

INTERPOLL LABORATORIES, INC.

Daniel Despen,
Manager

Stationary Source Testing Department

