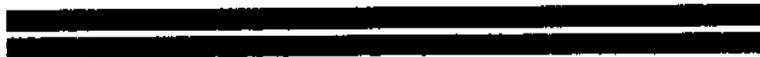


Note: This is a reference cited in AP 42, *Compilation of Air Pollutant Emission Factors, Volume I Stationary Point and Area Sources*. AP42 is located on the EPA web site at [www.epa.gov/ttn/chief/ap42/](http://www.epa.gov/ttn/chief/ap42/)

The file name refers to the reference number, the AP42 chapter and section. The file name "ref02\_c01s02.pdf" would mean the reference is from AP42 chapter 1 section 2. The reference may be from a previous version of the section and no longer cited. The primary source should always be checked.

VOLATILE ORGANIC COMPOUND  
AND  
PARTICULATE EMISSION TESTING  
AT  
LOUISIANA-PACIFIC CORPORATION  
HOULTON, MAINE

**APCC** AIR POLLUTION  
CHARACTERIZATION  
AND CONTROL, LTD.



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VOLATILE ORGANIC COMPOUND  
AND  
PARTICULATE EMISSION TESTING  
AT  
LOUISIANA-PACIFIC CORPORATION  
HOULTON, MAINE

Prepared by:

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Principal Scientist

John H. Powell  
Principal

July 1996

APCC Project 96053

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**EXECUTIVE SUMMARY**

Air Pollution Characterization and Control, Ltd. (APCC) was retained by Louisiana-Pacific Corporation (Louisiana-Pacific) to provide Emissions Testing and Air Quality Engineering Services at their Houlton, Maine facility. The purpose of this project was to perform source emission measurements in order to calculate the VOC emissions and capture and control efficiency (CE). In addition, particulate matter (PM) emissions were determined in accordance with EPA Method 5 and NSPS Test Method 202 for front half PM (Method 5) and filterable PM including organic and inorganic condensables (Method 202). The testing was completed at the inlet (outlets of the surface and core dryer's primary cyclones) and outlet (stack) of the regenerative thermal oxidizer (RTO) for the following pollutants and diluents:

Particulate	RTO Stack
VOC	RTO Stack, Surface & Core Dryers
O <sub>2</sub> and CO <sub>2</sub>	RTO Stack

The table below is a summary of the PM emissions test program which shows compliance with the Maine Department of Environmental Protection (ME DEP) permitted PM emission standard of 0.02 gr/dscf and 15.66 lb/hr from the combined dryer sources while operating at a rate sufficient to maintain press production within 90% of the maximum rate of 21.6 tph.

**PARTICULATE EMISSION TESTING  
Louisiana-Pacific Corporation  
9 July 1996**

	<b>AVERAGE EMISSIONS</b>	<b>EMISSIONS STANDARD</b>
RTO Stack M-5	0.3 lb/hr	15.66 lb/hr
RTO Stack M-202	4.46 lb/hr*	15.66 lb/hr
RTO Stack M-5 & 202	4.64 lb/hr*	15.66 lb/hr

Note: \* = Average includes only test Runs 2 and 3. See Section 2.1 for discussion.

The table below is a summary of the Volatile Organic Compound (VOC) emissions test program for the RTO Stack which shows compliance with the ME DEP VOC emission standard of 5.61 lb/hr and 95% capture and control efficiency (CE).

**VOC EMISSION TESTING ON THE RTO STACK**

	<b>AVERAGE EMISSIONS</b>	<b>EMISSIONS STANDARD</b>
RTO Stack	0.95 lb/hr	5.61 lb/hr
RTO CE	96.1%	95%

## 1.0 INTRODUCTION

Air Pollution Characterization and Control, Ltd. (APCC) was retained by Louisiana-Pacific Corporation (Louisiana-Pacific) to provide Emissions Testing and Air Quality Engineering Services at their Houlton, Maine facility. The purpose of this project was to perform source emission measurements in order to calculate the VOC emissions and capture and control efficiency (CE) as well as the particulate matter (PM) emission rate. Volatile Organic Compound (VOC) testing was performed in accordance with EPA Method 25A to demonstrate compliance with the standards for VOC emissions at the facility. Additionally, APCC performed testing to demonstrate compliance with the particulate matter (PM) standard in accordance with EPA Method 5 and NSPS Test Method 202 for front half PM (Method 5) and filterable PM including organic and inorganic condensables (Method 202) for the RTO stack.

This report prepared by APCC details the methodology that APCC used to determine compliance with the permitted standards for VOC and particulate matter.

This test program was performed on 9 July 1996 by Bruce A. Henning Principal Scientist at APCC, who served as the Project Engineer and a staff of APCC Engineers and Environmental Technicians. Process operations and site coordination was supplied by Mark Stile, Environmental Manager of Louisiana-Pacific.

Section 2 of this report presents the results and discussion and Section 3 contains a process description of the facility including the process data recorded during the test program. Section 4 details the test methods used during the test program. Section 5 contains APCC's quality assurance/quality control guidelines as implemented for this test program.

## 2.0 RESULTS AND DISCUSSION

This section details the results and discussion of the compliance program with regards to the compliance with the permitted standards for VOC and PM. The results are discussed as applicable to both the ME DEP Air Emissions License No. A-327-72-G-M and the US EPA Clean Air Act Consent Decree entered into with Louisiana-Pacific on 30 September 1993.

### 2.1 RTO Stack Particulate Matter Emissions

Compliance PM emissions testing was performed at the Louisiana-Pacific facility located in Houlton, Maine on 9 July 1996. Sampling was performed at the exhaust stack of the RTO. Testing was performed to determine emission concentrations and the emission rates in accordance with EPA Method 5 and NSPS Test Method 202 for front half particulate matter (Method 5) and filterable particulate matter including organic and inorganic condensables (Method 202).

Louisiana-Pacific's Air Emissions License No. A-327-72-G-M requires that the filterable (front half) emissions from the RTO stack be less than 0.02 gr/dscf and 15.66 lb/hr. The PM testing program was completed with both the surface and core dryer units operating at a rate sufficient to maintain press production within 90% of the maximum rate of 21.6 tph. The emission rate was determined to be in compliance at 5.4% of the allowable 15.66 lb/hr with a total emission rate of 0.30 lb/hr and a PM concentration of 5.43E-04 gr/dscf. A summary of each of the PM test results based on the filterable (front half) emissions from the RTO stack is presented below in summary Table 2-1.

Table 2-1  
Data Summary for Method 5 PM on the RTO Stack

Louisiana-Pacific  
Houlton, Maine

TEST NUMBER: DATE: TIME:		1 7/9/96 1515-1615	2 7/9/96 1730-1900	3 7/9/96 1955-2055	AVERAGE
<b>PROCESS CONDITIONS</b>	<b>UNITS</b>				
Press Production Rate	tph	19.4	19.4	19.4	19.4
<b>SAMPLE CONDITIONS</b>					
Meter Volume	dscf	41.1	42.6	42.6	42.1
Isokinesis	%	95.3	98.1	99.7	97.7
Filterable Particulate Catch	mg	2.6	1.0	0.8	1.5
<b>STACK CONDITIONS</b>					
Stack Gas Flowrate	dscf/min	63,946	64,445	63,461	63,951
Average Stack Temperature	°F	258	257	256	257
Water Vapor in Stack Gas	% v/v	23.0	22.8	23.2	23.0
CO <sub>2</sub> in Stack Gas	%	3.7	5.9	4.5	4.7
O <sub>2</sub> in Stack Gas	%	16.5	16.1	15.9	16.0
<b>MEASURED EMISSIONS</b>					
Particulate Concentration	gr/dscf	9.77E-04	3.62E-04	2.90E-04	5.43E-04
Mass Emission Rate	lb/hr	0.54	0.20	0.16	0.30

Revised 8/30/96

Three 60-minute tests were performed on 9 July 1996 to determine emission concentrations of PM under press operating conditions which yielded 19.43 tons per hour or 90% of the maximum operating capacity. The emission concentration in grain per dry standard cubic feet (gr/dscf) averaged  $5.43E-04$  gr/dscf, below the 0.02 gr/dscf emission standard. The results for the three tests were 0.54, 0.20, and 0.16, pounds per hour (lb/hr) respectively. The average of the three tests was calculated to be 0.30 lb/hr. This represents 5.4 % of the total allowed emission rate of 15.66 lb/hr.

The oxygen levels varied from 3.7 % to 5.9 % for all three of the tests. Oxygen concentrations averaged 4.7 % for the entire test program. Emissions data summaries and copies of the Method 5 sheets as recorded during the test program are presented in Appendix C.

All three tests performed were within the  $100\% \pm 10\%$  isokinetic acceptable range as required by the reference method. Both the sampling and pitot leak checks were acceptable at less than 0.02 cfm.

The US EPA Clean Air Act Consent Decree entered into with Louisiana-Pacific on 30 September 1993 requires that the results be reported as total PM. Total PM was determined to have an emission rate of 4.64 lb/hr and a PM concentration of  $8.47E-03$  gr/dscf based on the average of Test Runs 2 and 3. Test Run 1 was discarded due to contamination as described below.

As seen in the tables below, Test Run 1 seems to be an outlier in the fact that total PM results are 4 times the average of Test Runs 2 and 3. The Run 1 condensable sample underwent further analysis by infrared (IR) scan to determine that silicone lubricant contamination contributed to the high results. Therefore, Run 1 is not included in the average reported CPM results. The Interpoll Laboratory's analytical data is presented in Appendix G.

A summary of each of the additional condensable PM results is presented in Tables 2-2 and 2-3. All associated field data and detailed summaries are presented in Appendix B of this report.

## 2.2 VOC Emissions and RTO Capture Efficiencies

This section presents a discussion of test data collected during each VOC emission test. APCC performed three 60 minute tests on the RTO stack and the outlets from the surface and core dryer primary cyclones which served as the inlets to the RTO for the calculation of the RTO's CE. These tests were performed at the same time as the PM tests under the same operating conditions as described above, detailed in Section 3 and presented in Appendix E, pages 2 and 3. A results summary for each test run is presented in Table 2-4. Complete tabulated data for each test is presented in Appendix B.

**Table 2-2**  
**Data Summary for Filterable PM Containing Organic Condensables**  
**Louisiana-Pacific**  
**Houlton, Maine**

TEST NUMBER:		1	2	3	
DATE:		7/9/96	7/9/96	7/9/96	
TIME:		1515-1615	1730-1900	1955-2055	
PROCESS CONDITIONS	UNITS				AVERAGE
Press Production Rate	tph	19.4	19.4	19.4	19.4
<b>SAMPLE CONDITIONS</b>					
Meter Volume	dscf	41.1	42.6	42.6	42.6
Isokinesis	%	95.3	98.1	99.7	98.9
Condensable PM Catch	mg	92.0	23.0	22.0	22.5
<b>STACK CONDITIONS</b>					
Stack Gas Flowrate	dscf/min	63,946	64,445	63,461	63,953
Average Stack Temperature	°F	258	257	256	257
Water Vapor in Stack Gas	% v/v	23.0	22.8	23.2	23.0
CO <sub>2</sub> in Stack Gas	%	3.7	5.9	4.5	5.2
O <sub>2</sub> in Stack Gas	%	16.5	16.1	15.9	16.0
<b>MEASURED EMISSIONS</b>					
Particulate Concentration	gr/dscf	3.46E-02	8.33E-03	7.96E-03	8.15E-03
Mass Emission Rate	lb/hr	18.93	4.60	4.33	4.46

Note: Average includes only test Runs 2 and 3. See Section 2.1 for details.

**Table 2-3**  
**Data Summary for Total PM (M-5 & 202)**  
**Louisiana-Pacific**  
**Houlton, Maine**

TEST NUMBER:		1	2	3	
DATE:		7/9/96	7/9/96	7/9/96	
TIME:		1515-1615	1730-1900	1955-2055	
PROCESS CONDITIONS	UNITS				AVERAGE
Press Production Rate	tph	19.4	19.4	19.4	19.4
<b>SAMPLE CONDITIONS</b>					
Meter Volume	dscf	41.1	42.6	42.6	42.6
Isokinesis	%	95.3	98.1	99.7	98.9
Total Particulate Catch	mg	94.6	24.0	22.8	22.5
<b>STACK CONDITIONS</b>					
Stack Gas Flowrate	dscf/min	63,946	64,445	63,461	63,953
Average Stack Temperature	°F	258	257	256	257
Water Vapor in Stack Gas	% v/v	23.0	22.8	23.2	23.0
CO <sub>2</sub> in Stack Gas	%	3.7	5.9	4.5	5.2
O <sub>2</sub> in Stack Gas	%	16.5	16.1	15.9	16.0
<b>MEASURED EMISSIONS</b>					
Particulate Concentration	gr/dscf	3.55E-02	8.69E-03	8.25E-03	8.47E-03
Mass Emission Rate	lb/hr	19.47	4.80	4.49	4.64

Note: Average includes only test Runs 2 and 3. See Section 2.1 for details.

Table 2-4

Data Summary for VOC Emissions and CE  
Louisiana-Pacific, Houlton, Maine

	EMISSION RATES				CAPTURE EFFICIENCY (CE) %
	INLET SITE 1 lbs/hr	INLET SITE 2 lbs/hr	INLET 1 & 2 lbs/hr	OUTLET SITE 4 lbs/hr*	
Test 1 Average	9.7	15.6	25.3	0.7	97.4
Test 2 Average	9.2	13.1	22.4	1.5	93.4
Test 3 Average	10.9	16.5	27.4	0.7	97.5
<b>TEST PROGRAM AVERAGES</b>			<b>25.0</b>	<b>0.9</b>	<b>96.1</b>
<b>VOC Limit = 5.61 lbs/hr*</b>					

The average test program VOC emission rate at the RTO stack outlet was determined to be 0.9 lb/hr, which is 16% of the ME DEP permitted emission standard of 5.61 lb/hr. The VOC concentrations at the RTO stack ranged from 0.4 ppm to 18.2 ppm, while the test program average was 4.6 ppm.

The following equation was used to calculate VOC lbs/hr emissions.

$$\text{lbs/hr} = (\text{ppm}) * (\text{Conversion Factor}) * (Q_s, \text{scfm}) * (60 \text{ min. /hr})$$

where: Conversion Factor = THC as methane = 4.149E-08  
 $Q_s$  = standard flow, scf/min

The sum of the results from Sites 1 and 2, after the primary cyclones were used to determine the VOC contribution from the dryers. The CE of the pollution control system, the RTO was calculated as follows:

$$\text{VOC EFFICIENCY} = 1 - ((\text{VOC @ Site 4}) / (\text{VOC @ Site 1} + \text{VOC @ Site 2})) * 100$$

As can be seen from the table presented above the test program average CE was calculated to be 96.1%. The three test averages were 97.4, 93.4, and 97.5 % for tests 1, 2, and 3 respectively.

### 3.0 PROCESS AND OPERATIONS

The Louisiana-Pacific facility in Houlton Maine is an oriented strand board manufacturing facility that produces structural panel used for various construction applications. The facility is identified by the Standard Industrial Classification Code 2493. A complete process flow diagram is presented in Appendix A.

The plant purchases logs that are debarked and fed to a waferizer. The bark is used for fuel in the thermal oil heater. The waferizer flakes the logs into thin pieces, which are approximately three inches long by one inch wide by 1/32 inch thick. The freshly cut pieces have a moisture content of approximately 50%. The wet flakes go through a rotary dryer which reduces the moisture content to between four and eight percent. The flakes are then captured by the primary cyclone and the exhaust gas passes through a wet electrostatic precipitator (ESP) followed by a regenerative thermal oxidizer (RTO).

The flakes collected by the primary cyclone drop into a rotary screen, which separates the correctly sized flakes for further processing. The material passing through the screen is used as fuel in the dryer. Wax and resin are mixed with the flakes in rotary blenders. Formers then evenly distribute the flakes onto a moving conveyer. A separate former is used to orient the bottom, core and top layers of the board. The continuous mat of flakes is separated into press size segments by the flying cut-off saw.

The loader loads the boards into the press and with the combination of heat (supplied by the thermal oil heater) and pressure, the wafer mats are turned into solid boards. These boards are unloaded and cut by the trim saw to the desired sizes. The dust formed by this operation is collected and used as fuel in the wafer dryer.

The facility operates several pollution control devices to control emissions. As mentioned above, the rotary dryer exhaust is controlled by a wet ESP and the RTO. Emissions generated by the thermal oil heater pass through a cyclone and ESP. Emissions from the board press are controlled by a RTO.

#### 3.1 Process Equipment Description and Operating Conditions

The description of the process equipment that was tested is two MEC model 1248 T triple pass rotary drum wafer dryers with rated capacities of 230 tons per hour (tph) of wafers at six percent moisture. The primary burners are McConnell model 48 wood fired cyclonic suspension burners with rated capacities of 40 MM Btu/hr.

The dryers were operated at a rate sufficient to maintain press production within 90% of the maximum rate of 21.6 tph of finished product. The actual press production rate was maintained at 90 % with a rate of 19.4 tph.

The dryers' McConnell burners used dry fines as fuel during the testing. The fuel counts were recorded during the test program and are presented in Appendix E. The counts were factored based on the current quarterly fuel calibration to obtain the pounds of fuel burned. Wafers were dried to 4.5% - 5.5% moisture by weight. The

dryer operating parameters were recorded at ten minute intervals and are presented in detail in Appendix D. Dryer production rate in pounds of dry furnish per hour was determined based on the press production plus screened fines and board trim using the following formula:

$$\text{lb Dryer Production/Hr} = \frac{(\text{Tons press production/Hr}) / 2000}{1 - (0.07 + 0.08)}$$

where: Board trim = 7 % of finished product weight  
 screened fines = 8 % of finished product weight

### 3.2 Control Equipment Description and Operating Conditions

Emissions from the dryers are controlled by a wet electrostatic precipitator (ESP) manufactured by Geoenergy model 1013-378 2 T/R GEOENERGY E-Tube<sup>®</sup> followed by a Wheelabrator Clean Air Systems Inc. model No. 9220-7-95-04/96 regenerative thermal oxidizer (RTO). Operating specifications of the wet ESP include:

- Primary and secondary volts > 40 KV;
- Primary and secondary amperes 150-300 mA;
- Number of fields on line: 2;
- Flue gas conditioning: Saturation of gas stream; and
- Voltages, amperes flush cycles, and blowdown information.

Operating specifications of the RTO include:

- Combustion temperature: >1500 °F; and
- Primary fuel: Propane.

The test program averages are presented in Table 3-1 and further detailed in Appendix E, pages 2 and 3.

Table 3-1  
 Process Data Summary  
 Louisiana-Pacific, Houlton, Maine

PROCESS CONDITION	UNITS	PROGRAM AVERAGE
Press Production Rate	tph	19.43
Dryers' Production Rate	lb/hr	44,597
Total Fuel Burned	tph	2.87
Incoming Moisture	%	33.05
Dry Moisture	%	6.17
Inlet Temperature	°F	1,168
RTO Temperature No. 1	°F	1,507
RTO Temperature No. 2	°F	1,510
RTO Temperature No. 3	°F	1,510

## 4.0 SAMPLING AND ANALYTICAL METHODOLOGY

APCC mobilized two Environmental Monitoring Laboratories (EML) and other test equipment at the test site. Upon arrival, APCC met with the project management supervisor and site coordinator familiarizing themselves with the facility, safety procedures, and process operations. The following sections present brief descriptions of the sampling and analytical methodologies.

### 4.1 Continuous Emission Monitoring

APCC performed continuous emission monitoring to determine emissions of carbon dioxide (CO<sub>2</sub>), oxygen (O<sub>2</sub>), and Volatile Organic Compounds (VOC) in accordance with EPA Methods 3A and 25A. All CEM data was recorded using Tracor/Westronics 3000 automatic digital data loggers. Copies of the strip chart recordings are presented in Appendix D.

The CEM systems housed in the APCC EMLs were located at the base of the RTO stack and below Sites 1 and 2. In each system stack gas was drawn through an in-stack filter, a heated stainless steel heated probe, heated Teflon sample line (320°F nominal), the VOC sample was drawn directly from the heated sample line into the VOC analyzer for analysis on a wet basis. A portion of the sample was split at the back of the VOC analyzer and drawn through a Peltier-type sample conditioner by a leakless Teflon diaphragm pump. The sample was then pumped through a manifold under slightly positive pressure with a bypass to atmosphere. CO<sub>2</sub> and O<sub>2</sub> samples were continuously drawn from this manifold to their respective analyzers. The VOC sample bypassed the condenser system and was passed directly to the analyzer. A schematic of the APCC's instrument reference method (IRM) monitoring systems is presented in the Figure 4-1.

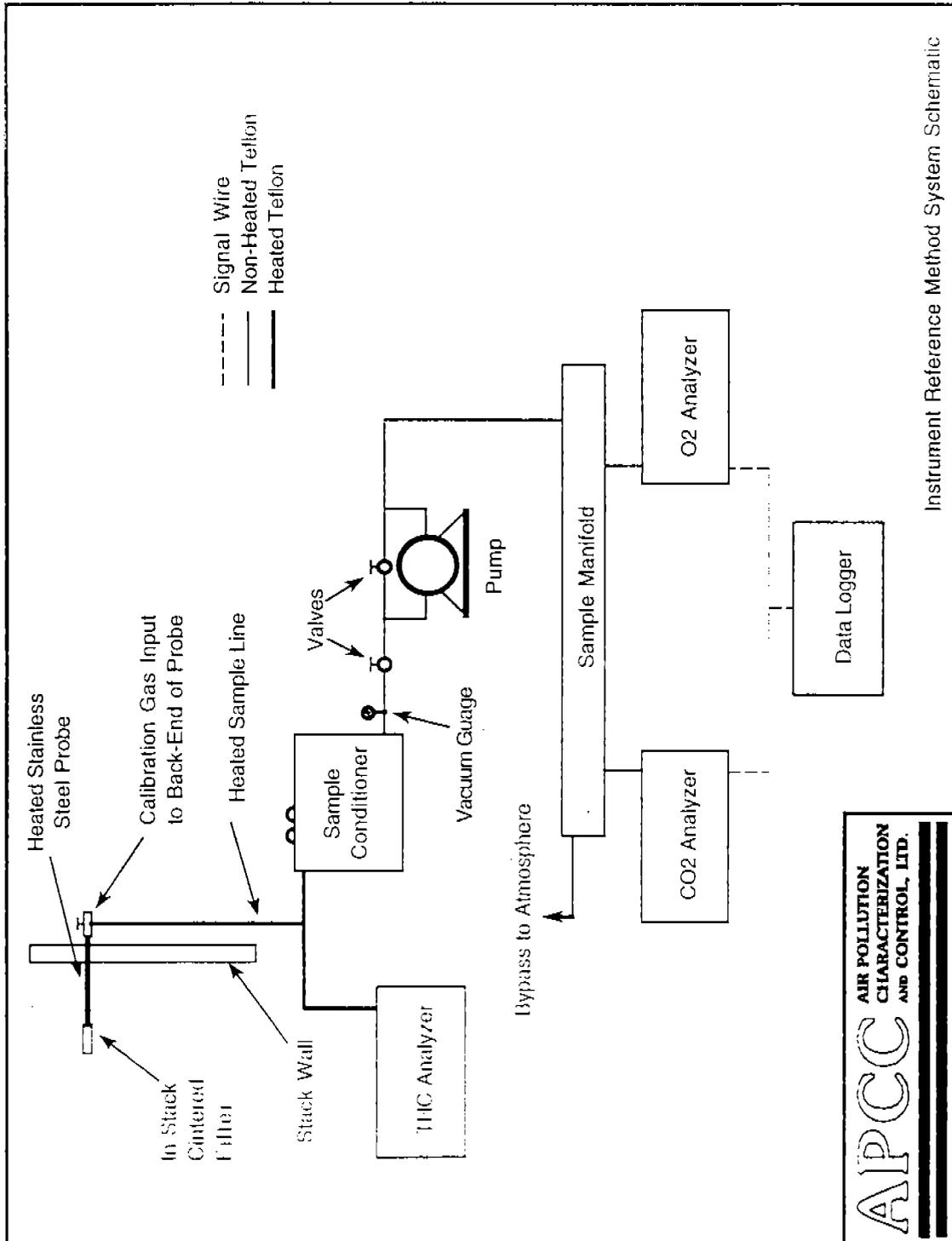
#### **4.1.1 Volatile Organic Compound Analyzers**

A VIG Industries dual channel total hydrocarbon analyzer, which utilizes two flame ionization detectors (FIDs) to measure, as methane, hydrocarbons C<sub>1</sub> through C<sub>18</sub>; was used to sample from the outlets of Sites 1 and 2 the surface and core dryers simultaneously with the TECO Model 51 Total Hydrocarbon Analyzer. Approximately 5.0 lpm of sample gas is drawn from the sample locations through Teflon sample line heated to 350°F (nominal). The sample gas is drawn through a heated filter and valving by a heated pump. The sample gas then enters the heated detector bench which contains the FID.

#### **4.1.2 Oxygen Analyzers**

A Westinghouse/Maihak OXIGOR O<sub>2</sub> analyzer calibrated on the 0-25% scale was used to monitor concentrations of oxygen in the exhaust stream. This instrument utilizes the magnetic dumbbell sphere (paramagnetic) principle, which comparatively measures the magnetic susceptibility of a gas volume by the force acting upon a non-magnetic test body suspended in a disproportionate magnetic field. Output current is linearly proportional to the oxygen concentration.

Figure 4-1 APCC IRM System Schematic



A Teledyne 326RA series analyzer was also used in the other EML to monitor O<sub>2</sub> concentrations in a gas stream. This instrument utilizes a micro fuel cell to measure oxygen content. Output voltage is linearly proportional to the oxygen concentration in the sample stream. This analyzer was calibrated on the 0-25% scale.

#### 4.1.3 Carbon Dioxide Analyzers

A Westinghouse/Maihak FINOR CO<sub>2</sub> analyzer was used to monitor carbon dioxide emissions in EML No. 1. This instrument operates on the principle of carbon dioxide having a known characteristic absorption spectra in the infrared range.

In addition, a Westinghouse Model UNOR 6N non-dispersive infrared gas analyzer was used to measure CO<sub>2</sub> concentrations. The analyzer operates on the measurement principle based on CO<sub>2</sub> having a known characteristic absorption spectra in the infrared range. It contains an infrared detector that uses the non-dispersive single beam technique with alternative modulation of the sample and reference cells. Radiation absorbed by CO<sub>2</sub> in the sample cell produces a capacitance change in the detector which is proportional to the CO<sub>2</sub> concentration. Both the CO<sub>2</sub> were calibrated on the 0-25% scale.

#### 4.1.4 Calibration

Four point (zero, low, mid and span) calibrations for hydrocarbons and three point (zero, mid and span) calibrations for other parameters were performed on the analytical instrumentation at the beginning of the test program to establish instrument linearity. A zero and span calibration on each instrument was performed before and after each test. The system was also leak and bias checked prior to the test program. EPA Protocol 1 gases were used for all calibrations.

#### 4.1.5 Data Acquisition and Handling

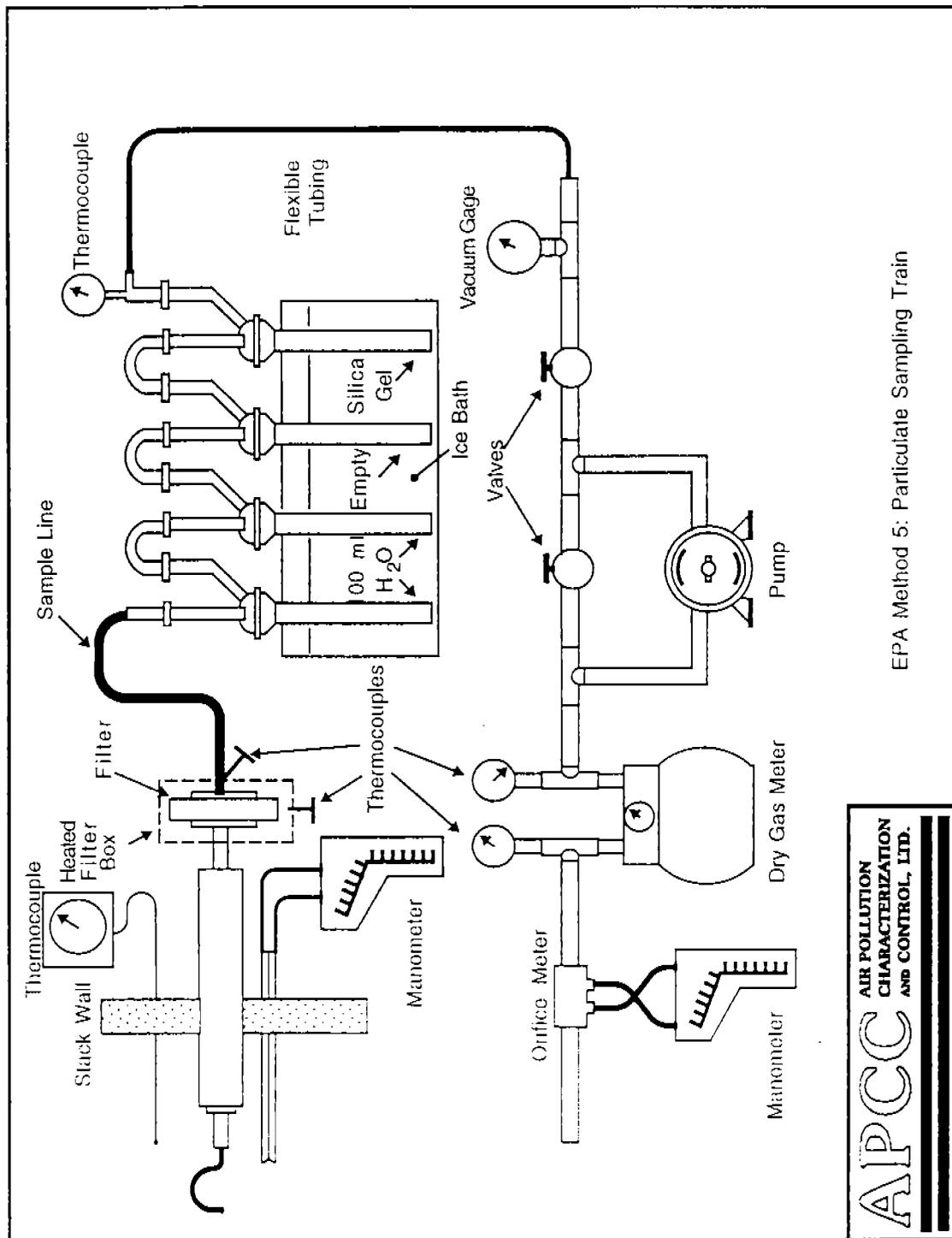
All CEM data was monitored by a Tracor/Westronics 3000 digital data loggers which recorded on a strip charts using its integral color printer. Trends were monitored using the strip chart mode with averages printed digitally for 10-minute intervals. Emission data are "viewed" by the data logger at 5-second intervals. This enables real-time emission data to be available on-site.

### 4.2 Particulate Emission Measurements

Particulate sampling was performed in accordance with EPA Method 5, as described in the July 1, 1995 edition of the *Code of Federal Regulations* (CFR). In addition, NSPS Test Method 202 for front half PM (Method 5) and filterable PM including organic condensable (Method 202) was completed. Triplicate 60-minute tests were performed at all three sites. However, for the purposes of this compliance report only the Site 4 PM data is reported.

A schematic of the sampling train similar to the one that was used during testing is presented in Figure 4-2. The RTO stack particulate sampling was performed in

Figure 4-2 EPA Method 5 Sampling Train



EPA Method 5: Particulate Sampling Train

**APCC**  
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accordance with a EPA Method 5, as described in the July 1, 1995 edition of the *Code of Federal Regulations* (CFR). The particulate sampling train consisted of a nozzle attached to a glass-lined probe which is heated to prevent condensation. Whatman EPM 2000 fiberglass filter paper supported in a 4-1/2 inch glass filter holder was used as the collection media. The filter assembly will be enclosed in a heated box to maintain temperatures at  $248^{\circ}\text{F} \pm 25^{\circ}\text{F}$ . A thermocouple located inside the back half of the filter holder, was used to monitor the gas stream temperature and verify that the temperature is kept at  $248^{\circ}\text{F} \pm 25^{\circ}\text{F}$ .

An ice bath containing four impingers was attached to the back end of the filter via a flexible umbilical tube. The first, third, and fourth impingers were of modified Greenburg-Smith design, while the second will be the standard Greenburg-Smith design. The first two impingers contained 100 ml distilled water, the third is dry, and the fourth contains 200 grams of indicating silica gel to remove any remaining moisture. Flexible tubing, vacuum gauge, needle valves, leakless vacuum pump, bypass valve, dry gas meter, calibration orifice and inclined manometer complete the sampling train. The stack velocity pressure was measured using a pitot tube and inclined manometer in accordance with EPA Method 2. The stack temperature was monitored using a calibrated K-type thermocouple connected to a potentiometer.

A nomograph was used to quickly determine the orifice pressure drop required for a pitot velocity pressure and stack temperature in order to maintain isokinetic sampling conditions. Sampling flow was adjusted by means of the bypass valve. Before and after each particulate test run, the sampling train was leak checked and acceptable at less than 0.02 cubic feet per minute (cfm). The moisture content of the exhaust gases was determined during each test in accordance with EPA Method 4. Test data was recorded on field data sheets as presented in Appendix C of this report.

#### Sample Recovery:

At the end of each test, three sample containers were used as follows:

- |                 |  |
|-----------------|--|
| Container No. 1 | Filter   |
| Container No. 2 | Acetone wash of probe and front half of filter. The probe and nozzle will be washed and brushed three times. |
| Container No. 3 | Silica gel from the fourth impinger.   |

#### Sample Analysis:

The samples were transported to the laboratory and the following analyses performed:

- |                 |   |
|-----------------|---|
| Container No. 1 | Transfer the filter and any loose particulate matter from the sample container into a desiccator and dry for approximately 24 hours. The sample is then weighed to a constant weight. Reported results to the nearest 0.1 mg. |
|-----------------|---|

- Container No. 2     The acetone washing will be transferred to a tared beaker and evaporated to dryness. Desiccated and dried to a constant weight. Reported results to the nearest 0.1 mg.
- Container No. 3     Silica gel will be weighed to the nearest 0.5 g. The weight of the moisture entrapped in the silica gel, along with the volume of moisture which condensed in the impingers, will be used to calculate the moisture content of the flue gas.

A computer program developed for the Macintosh was used to calculate emission rates in grains per dry standard cubic foot (gr/dscf) and pounds per hour (lb/hr). The program was also calculate percent moisture, molecular weight of the stack gas at stack conditions, and the percent isokinisis.

#### **4.3 Volumetric Flow Rate Determination and Sampling Locations**

Exhaust gas volumetric flow rate was determined at the inlets and outlet of the RTO in conjunction with each of the VOC emission tests in accordance with EPA Methods 1 and 2 which were performed in conjunction with the PM tests completed at all three locations.

Two sample ports at Site 1 are located at 90° of one another in the exhaust from the surface dryer 25 ft or 7.1 diameters upstream and 45 ft or 12.6 diameters downstream from the nearest respective flow disturbances in the 42 inch diameter duct.

Two sample ports at 90° of one another in the 42 inch diameter core dryer duct at Site 2 are located at 29 ft or 8.3 diameters upstream and 29 ft or 8.3 diameters downstream from the nearest disturbances.

In accordance with EPA Method 1, 12 traverse points were measured at Sites 1 and 2 to determine stack gas velocity and temperature.

The RTO stack sampling location was on the platform at the 60 ft elevation. The two sampling ports are located in the 82 inch stack at 36 ft or 5.3 diameters upstream and 40 ft or 5.6 diameters downstream from the nearest disturbances. Therefore, in accordance with EPA Method 1, 20 traverse points were measured to determine stack gas velocity and temperature.

Appendix A presents diagrams of each sampling location. Appendix C details the velocity and Method 5 traverse points used at each sampling location.

## 5.0 QUALITY ASSURANCE

The project manager is responsible for implementation of the quality assurance program as applied to the project.

### 5.1 Sampling Quality Assurance

Generally, implementation of quality assurance procedures for source measurement programs is designed so that the work is done:

1. By competent, trained individuals experienced in the specific methodologies being used.
2. Using properly calibrated equipment.
3. Using approved procedures for sample handling and documentation.

Measurement devices, pitot tubes, dry gas meters, thermocouples, etc. are uniquely identified and calibrated with documented procedures and acceptance criteria before and after each field effort. Records of all calibration data are maintained in the files.

Data are recorded on standard forms. Bound field notebooks are used to record observations and miscellaneous elements affecting data, calculations, or evaluation.

Specific details of APCC's QA program for stationary air pollution sources may be found in "Quality Assurance Handbook for Air Pollution Measurement Systems", Volume III (EPA-600/4-7-027b).

### 5.2 Equipment Calibration

The CEM system was calibrated at the beginning and end of each test day as well as leak and biased checked before and after each test. All calibration gases were EPA Protocol 1. Multi-point calibrations were performed to established linearity prior to sampling and throughout the test program. Appendix B presents the EML CEM work sheets which include all of the calibration data and bias corrections. All of the calibrations met the specifications of EPA Method 6C Section 8.

### 5.3 Data Reduction and Reporting

The Project Engineer developed a data reduction system to conform to the collection of field data to be reduced and quantitative results for the final report. The methods for data reduction were specified and presented to the Program Manager before the field effort. Raw data recorded on field data sheets, bound laboratory books, and data logger strip charts are presented in the Appendix of this report.

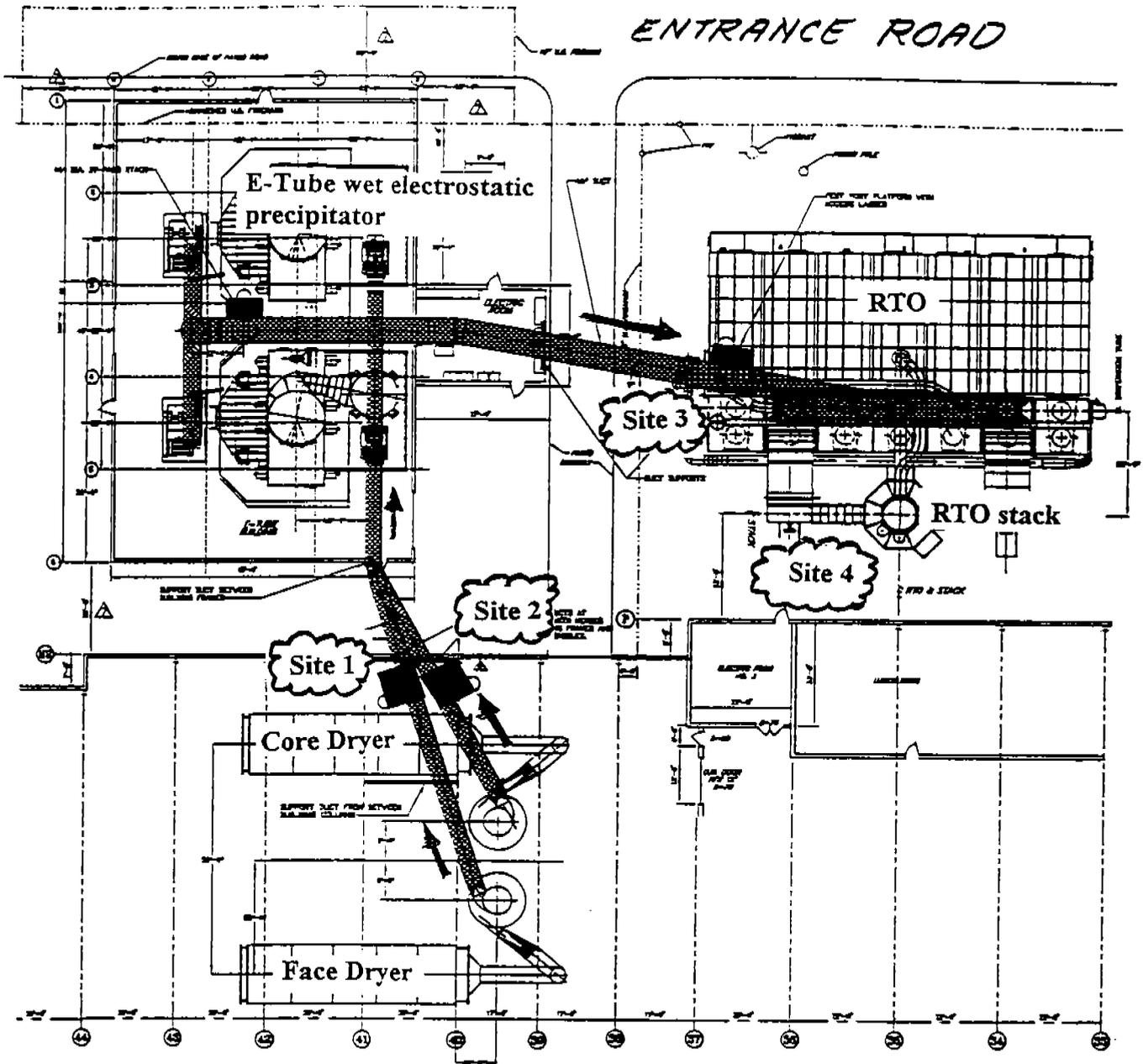
#### 5.4 Data Validation

Validation of data were reviewed by the Manager of Engineering and Company President against the QA/QC criteria of the specific methods. The data were assessed to the quality and accuracy as required to meet the objectives of the sampling program. Hand calculations were performed with raw data separate from the reported calculations and results. All documentation was checked for correctness, completeness and verified as checked.

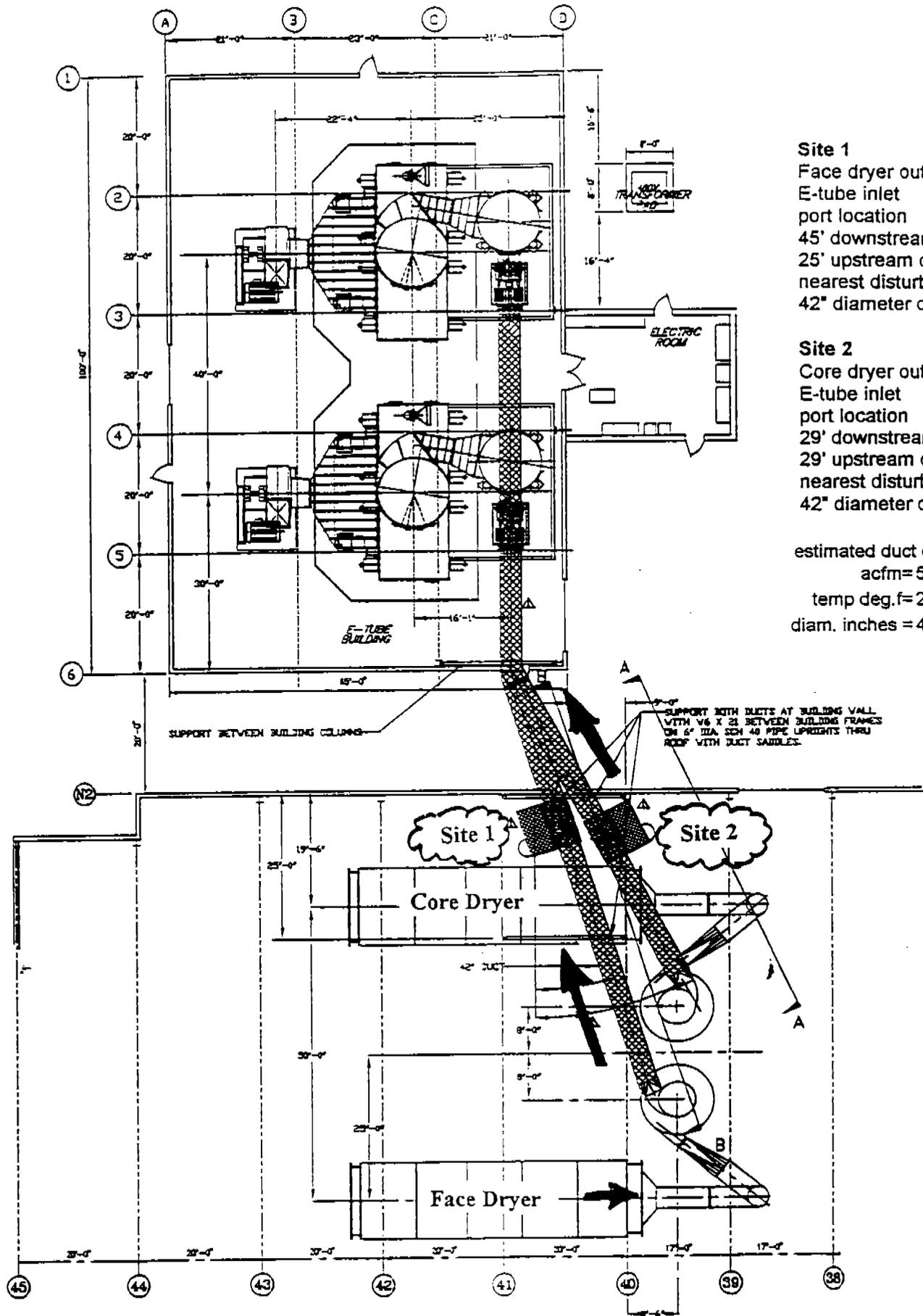
A data assessment of sampling results was also performed during scheduled time periods to ensure quality data is collected and processed. Corrective action was implemented if warranted to ensure QA/QC procedures are met. No corrective actions were necessary.

**APPENDIX A**  
**Process Flow Chart**  
**&**  
**Sampling Location Diagrams**





A-3 Plan view of dryer, control equipment and test port locations



**Site 1**  
 Face dryer outlet  
 E-tube inlet  
 port location  
 45' downstream and  
 25' upstream of  
 nearest disturbance  
 42" diameter duct

**Site 2**  
 Core dryer outlet  
 E-tube inlet  
 port location  
 29' downstream and  
 29' upstream of  
 nearest disturbance  
 42" diameter duct

estimated duct conditions  
 acfm= 50000  
 temp deg.f= 240  
 diam. inches = 42"

SUPPORT BOTH DUCTS AT BUILDING WALL  
 WITH V6 X 21 BETWEEN BUILDING FRAMES  
 ON 6" DIA. SCH 40 PIPE UPRIGHTS THRU  
 ROOF WITH DUCT SADDLES.

A-4 Detail of port locations 1 and 2- dryer outlet:



**APPENDIX B**  
**Results Summaries**

CLIENT:	LOUISIANA PACIFIC						
LOCATION:	SITE 4 (RTO STACK)						
PROJECT NUMBER:	96053						
TEST NUMBER:							
DATE:	1	2	3				AVERAGE
TIME :	7/9/96	7/9/96	7/9/96				
	1515-1615	1730-1900	1955-2055				

TEST DATA INPUT	SYMBOL	UNITS				
Barometric Pressure	Pbar	in. Hg	29.88	29.88	29.88	
Stack Area	A	ft <sup>2</sup>	36.7	36.7	36.7	
Nozzle Diameter (in.)	Dn	in.	0.275	0.275	0.275	
Total Sampling Time	Ø	min.	60	60	60	
Calibration Factor	Y	-	1	1	1	
Pitot Coefficient	Cp	-	0.84	0.84	0.84	
Average Square Root of Velocity Head	$\sqrt{\Delta P_{avg}}$	in. H <sub>2</sub> O	0.753	0.76	0.749	
Average Orifice Pressure Drop	ΔH	in. H <sub>2</sub> O	2.01	2.04	2	
Average Meter Temperature	Tm	°F	84	80	78	
Average Stack Pressure	Pg	in. H <sub>2</sub> O	0.57	0.56	0.57	
Average Stack Temperature	Ts	°F	258	257	256	
Meter Volume @ Meter Conditions	Vm	ft <sup>3</sup>	42.16	43.41	43.28	
Total Water Collected	Vlc	ml	261	267	274	
CO <sub>2</sub> in Stack Gas	CO <sub>2</sub>	%	3.7	5.9	4.5	
O <sub>2</sub> in Stack Gas	O <sub>2</sub>	%	16.5	16.1	15.9	
CO in Stack Gas	CO	%	0	0	0	
Total Filtered Particulate Catch	PMT	mg	2.6	1.0	0.8	1.5

CALCULATED VALUES						
Meter Volume	Vmstd	dscf	41.1	42.6	42.6	42.1
Water Vapor in Stack Gas	Bws	%	23.03	22.78	23.23	23.01
Molecular Weight of Stack Gas (dry)	Md	g/g-mole	29.3	29.6	29.4	29.4
Molecular Weight of Stack Gas (wet)	Ms	g/g-mole	26.7	26.9	26.7	26.8
Average Velocity of Stack Gas	Vs	ft/min	3,078	3,088	3,054	3,073
Actual Stack Gas Flowrate	Q	acf/min	112,963	113,326	112,086	112,792
Stack Gas Flowrate	Qsd	dscf/min	63,946	64,445	63,461	63,951
Isokinetics	I	%	95.3	98.1	99.7	97.7

EMISSION CONCENTRATION						
Particulate Emission Concentration	PCgr	gr/acf	7.18E-04	2.67E-04	2.14E-04	4.00E-04
Particulate Emission Concentration	PCgrsd	gr/dscf	9.77E-04	3.62E-04	2.90E-04	5.43E-04
Particulate Emission Concentration	PClbsd	lb/dscf	1.39E-07	5.17E-08	4.13E-08	7.75E-08
Particulate Emission Concentration	PCµgm	µg/dscm	2237	829	663	1243

EMISSION RATE						
Particulate Emission Rate	PER	lbs/hr	0.54	0.20	0.16	0.30

CLIENT:		LOUISIANA PACIFIC					
LOCATION:		SITE 4 (RTO STACK)					
PROJECT NUMBER:		96053					
TEST NUMBER:				1	2	3	AVERAGE
DATE:				7/9/96	7/9/96	7/9/96	
TIME :				1515-1615	1730-1900	1955-2055	
<b>TEST DATA INPUT</b>							
Barometric Pressure	Pbar	in. Hg	29.88	29.88	29.88		
Stack Area	A	ft <sup>2</sup>	36.7	36.7	36.7		
Nozzle Diameter (in.)	Dn	in.	0.275	0.275	0.275		
Total Sampling Time	Ø	min.	60	60	60		
Calibration Factor	Y	-	1	1	1		
Pitot Coefficient	Cp	-	0.84	0.84	0.84		
Average Square Root of Velocity Head	√ΔPavg	in. H <sub>2</sub> O	0.753	0.76	0.749		
Average Orifice Pressure Drop	ΔH	in. H <sub>2</sub> O	2.01	2.04	2		
Average Meter Temperature	Tm	°F	84	80	78		
Average Stack Pressure	Pg	in. H <sub>2</sub> O	0.57	0.56	0.57		
Average Stack Temperature	Ts	°F	258	257	256		
Meter Volume @ Meter Conditions	Vm	ft <sup>3</sup>	42.16	43.41	43.28		
Total Water Collected	Vlc	ml	261	267	274		
CO <sub>2</sub> in Stack Gas	CO <sub>2</sub>	%	3.7	5.9	4.5		
O <sub>2</sub> in Stack Gas	O <sub>2</sub>	%	16.5	16.1	15.9		
CO in Stack Gas	CO	%	0	0	0		
Total Condensible PM Catch	PMt	mg	92.0	23.0	22.0		22.5
<b>CALCULATED VALUES</b>							
Meter Volume	Vmstd	dscf	41.1	42.6	42.6		42.6
Water Vapor in Stack Gas	Bws	%	23.03	22.78	23.23		23.0
Molecular Weight of Stack Gas (dry)	Md	g/g-mole	29.3	29.6	29.4		29.5
Molecular Weight of Stack Gas (wet)	Ms	g/g-mole	26.7	26.9	26.7		26.8
Average Velocity of Stack Gas	Vs	ft/min	3,078	3,088	3,054		3071.0
Actual Stack Gas Flowrate	Q	acf/min	112,963	113,326	112,086		112706.2
Stack Gas Flowrate	Qsd	dscf/min	63,946	64,445	63,461		63952.9
Isokinetics	I	%	95.3	98.1	99.7		98.9
<b>EMISSION CONCENTRATION</b>							
Particulate Emission Concentration	PCgr	gr/acf	2.54E-02	6.13E-03	5.87E-03		6.00E-03
Particulate Emission Concentration	PCgrsd	gr/dscf	3.46E-02	8.33E-03	7.96E-03		8.15E-03
Particulate Emission Concentration	PClbsd	lb/dscf	4.93E-06	1.19E-06	1.14E-06		1.16E-06
Particulate Emission Concentration	PCµgm	µg/dscm	79161	19078	18237		18657.4
<b>EMISSION RATE</b>							
Particulate Emission Rate	PER	lbs/hr	18.93	4.60	4.33		4.46

NOTE: Average includes only Runs 2 and 3.

CLIENT:	LOUISIANA PACIFIC				
LOCATION:	SITE 4 (RTO STACK)				
PROJECT NUMBER:	96053				
TEST NUMBER:		1	2	3	AVERAGE
DATE:		7/9/96	7/9/96	7/9/96	
TIME :		1515-1615	1730-1900	1955-2055	

TEST DATA INPUT	SYMBOL	UNITS				
Barometric Pressure	Pbar	in. Hg	29.88	29.88	29.88	
Stack Area	A	ft <sup>2</sup>	36.7	36.7	36.7	
Nozzle Diameter (in.)	Dn	in.	0.275	0.275	0.275	
Total Sampling Time	∅	min.	60	60	60	
Calibration Factor	Y	-	1	1	1	
Pitot Coefficient	Cp	-	0.84	0.84	0.84	
Average Square Root of Velocity Head	√ΔPavg	in. H <sub>2</sub> O	0.753	0.76	0.749	
Average Orifice Pressure Drop	ΔH	in. H <sub>2</sub> O	2.01	2.04	2	
Average Meter Temperature	Tm	°F	84	80	78	
Average Stack Pressure	Pg	in. H <sub>2</sub> O	0.57	0.56	0.57	
Average Stack Temperature	Ts	°F	258	257	256	
Meter Volume @ Meter Conditions	Vm	ft <sup>3</sup>	42.16	43.41	43.28	
Total Water Collected	Vlc	ml	261	267	274	
CO <sub>2</sub> in Stack Gas	CO <sub>2</sub>	%	3.7	5.9	4.5	
O <sub>2</sub> in Stack Gas	O <sub>2</sub>	%	16.5	16.1	15.9	
CO in Stack Gas	CO	%	0	0	0	
Total Particulate Catch (PM & CPM)	PMt	mg	94.6	24.0	22.8	23.4

CALCULATED VALUES						
Meter Volume	Vmstd	dscf	41.1	42.6	42.6	42.6
Water Vapor in Stack Gas	Bws	%	23.03	22.78	23.23	23.0
Molecular Weight of Stack Gas (dry)	Md	g/g-mole	29.3	29.6	29.4	29.5
Molecular Weight of Stack Gas (wet)	Ms	g/g-mole	26.7	26.9	26.7	26.8
Average Velocity of Stack Gas	Vs	ft/min	3,078	3,088	3,054	3071.0
Actual Stack Gas Flowrate	Q	acf/min	112,963	113,326	112,086	112706.2
Stack Gas Flowrate	Qsd	dscf/min	63,946	64,445	63,461	63952.9
Isokinetics	I	%	95.3	98.1	99.7	98.9

EMISSION CONCENTRATION						
Particulate Emission Concentration	PCgr	gr/acf	2.61E-02	6.40E-03	6.09E-03	6.24E-03
Particulate Emission Concentration	PCgrsd	gr/dscf	3.55E-02	8.69E-03	8.25E-03	8.47E-03
Particulate Emission Concentration	PClbsd	lb/dscf	5.07E-06	1.24E-06	1.18E-06	1.21E-06
Particulate Emission Concentration	PCμgm	μg/dscm	81398	19907	18900	19403.7

EMISSION RATE						
Particulate Emission Rate	PER	lbs/hr	19.47	4.80	4.49	4.64

NOTE: Average includes only Runs 2 and 3.

CAPTURE EFFICIENCY  
DATA  
LOUISIANA-PACIFIC  
9 JULY 1996

	CONCENTRATIONS				FLOW				EMISSION RATES				CAPTURE EFFICIENCY %
	VOC IN SITE 1 ppm	VOC IN SITE 2 ppm	VOC OUT SITE 4 ppm		INLET SITE 1 scfm	INLET SITE 2 scfm	OUTLET SITE 4 scfm		INLET SITE 1 lbs/hr	INLET SITE 2 lbs/hr	INLET 1 & 2 lbs/hr	OUTLET SITE 4 lbs/hr	
Test 1 Average	114.8	184.9	3.3		33,900	33,751	81,266		9.7	15.6	25.3	0.7	97.4
Test 2 Average	94.9	152.9	7.2		39,100	34,488	82,031		9.2	13.1	22.4	1.5	93.4
Test 3 Average	107.0	192.1	3.4		40,844	34,464	80,984		10.9	16.5	27.4	0.7	97.5

TEST PROGRAM AVERAGE 96.1

EML  
CEM SHEET

SOURCE:	Louisiana-Pacific Corp.	TEST:	1
DATE:	7/9/96	COLLECTED	
METHOD:	3A, 7E, 10, & 25A	BY:	ED
UNIT:	Thermal Oxidizer Inlet Site 1	WITNESSED	
FUEL:	Propane	BY:	N/A
LOAD:	N/A		

STEP	DESCRIPTION	LIMIT	THC	NOx	CO	O2	CO2
1	RANGE		1000	250	1000	25.0	25.0
2	CAL GAS						
	ZERO		0	0	0	0	0
	LOW		283				
	MID	(bias cal. gas)	513	99	498	12.80	12.60
	SPAN		901	241	883	22.6	19.7
3	INT. LOCAL CAL		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		1.8	0.2	3.3	0.1	-0.1
	% ERROR	±2 (±5% for THC)	0.2%	0.1%	0.3%	0.4%	-0.4%
	LOW (PPM OR %)		284.0				
	% ERROR	±2 (±5% for THC)	0.1%				
	MID (PPM OR %)		512.5	97.5	512.5	13.0	12.7
	% ERROR	±2 (±5% for THC)	-0.1%	-0.6%	1.5%	0.8%	0.4%
	HIGH (PPM OR %)		908.9	242.7	882.9	22.5	19.6
	% ERROR	±2 (±5% for THC)	0.8%	0.7%	0.0%	-0.4%	-0.4%
4	INT. BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO		1.8	0.6	2.8	0.1	0.0
	CAL BIAS	±5%	0.0%	0.2%	-0.1%	0.0%	0.4%
	UPSCALE		284.0	97.0	512.3	12.8	12.6
	CAL BIAS	±5%	0.0%	-0.2%	0.0%	-0.8%	-0.4%
5	RESP. TIME (SEC)		30.0	30.0	15.0	15.0	10.0
6	FINAL BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		9.6	1.0	4.0	0.1	0.0
	DRIFT	±3%	0.8%	0.2%	0.1%	0.0%	0.0%
	CAL BIAS	±5%	0.8%	0.3%	0.1%	0.0%	0.4%
	UPSCALE (MID) (PPM OR %)		283.8	100.0	510.0	12.8	12.5
	DRIFT	±3%	0.0%	1.2%	-0.2%	0.0%	-0.4%
	CAL BIAS	±5%	0.0%	1.0%	-0.3%	-0.8%	-0.8%
7	AVG SYSTEM BIAS		THC	NOx	CO	O2	CO2
	ZERO		5.7	0.8	3.4	0.1	0.0
	UPSCALE		283.9	98.5	511.2	12.8	12.6

Test 1	Integrated Avg	THC	NOx	CO	O2	CO2
1515-1615						
	5	99.4	22.1	171.0	16.9	3.9
	10	91.7	23.9	168.5	17.0	3.8
	15	98.6	21.9	202.5	16.8	3.9
	20	105.7	21.1	212.4	16.8	3.9
	25	98.6	22.5	176.2	16.9	3.9
	30	121.3	19.7	247.0	16.6	4.2
	35	122.8				
	40	128.0				
	45	114.0				
	50	137.4				
	55	130.0				
	60	122.0				

RESULTS	THC	NOx	CO	O2	CO2
	(ppmwv as CH4)	(ppmdv)	(ppmdv)	(%)	(%)
TEST AVERAGE	114.1	21.9	196.3	16.8	3.9
BIAS CORRECTED	114.8	21.3	189.2	16.9	3.9
FLOWRATE (dscfm)	26,114				
FLOWRATE (scfm)	33900				
lbs/hr	9.70	4.00	21.55		

EML  
CEM SHEET

SOURCE: Louisiana-Pacific Corp.	TEST: 2
DATE: 7/9/96	COLLECTED
METHOD: 3A, 7E, 10, & 25A	BY: ED
UNIT: Thermal Oxidizer Inlet Site 1	WITNESSED
FUEL: Propane	BY: N/A
LOAD: N/A	

STEP	DESCRIPTION	LIMIT	THC	NOx	CO	O2	CO2
1	RANGE		1000	250	1000	25.0	25.0
2	CAL GAS						
	ZERO		0	0	0	0	0
	LOW		283				
	MID	(bias cal. gas)	513	99	498	12.80	12.60
	SPAN		901	241	883	22.6	19.7
3	INT. LOCAL CAL		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		1.8	0.2	3.3	0.1	-0.1
	% ERROR	±2 (±5% for THC)	0.2%	0.1%	0.3%	0.4%	-0.4%
	LOW (PPM OR %)		284.0				
	% ERROR	±2 (±5% for THC)	0.1%				
	MID (PPM OR %)		512.5	97.5	512.5	13.0	12.7
	% ERROR	±2 (±5% for THC)	-0.1%	-0.6%	1.5%	0.8%	0.4%
	HIGH (PPM OR %)		908.9	242.7	882.9	22.5	19.6
	% ERROR	±2 (±5% for THC)	0.8%	0.7%	0.0%	-0.4%	-0.4%
4	INT. BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO		9.6	1.0	4.0	0.1	0.0
	CAL BIAS	±5%	0.8%	0.3%	0.1%	0.0%	0.4%
	UPSCALE		283.8	100.0	510.0	12.8	12.5
	CAL BIAS	±5%	0.0%	1.0%	-0.3%	-0.8%	-0.8%
5	RESP. TIME (SEC)		30.0	30.0	15.0	15.0	10.0
6	FINAL BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		11.3	0.4	2.3	0.2	0.1
	DRIFT	±3%	0.2%	-0.2%	-0.2%	0.4%	0.4%
	CAL BIAS	±5%	1.0%	0.1%	-0.1%	0.4%	0.8%
	UPSCALE (MID) (PPM OR %)		285.6	99.2	509.8	12.8	12.6
	DRIFT	±3%	0.2%	-0.3%	0.0%	0.0%	0.4%
	CAL BIAS	±5%	0.2%	0.7%	-0.3%	-0.8%	-0.4%
7	AVG SYSTEM BIAS		THC	NOx	CO	O2	CO2
	ZERO		10.5	0.7	3.2	0.2	0.1
	UPSCALE		284.7	99.6	509.9	12.8	12.6

Test 2	Integrated Avg	THC	NOx	CO	O2	CO2
1730-1905						
	5	110.5	25.4	206.3	16.7	4.0
	10	110.0	25.5	218.1	16.7	4.1
	15	61.6	24.1	104.4	17.4	3.3
	20	68.7	23.9	135.2	17.3	3.4
	25	78.7	23.0	157.8	17.1	3.5
	30	81.8				
	35	98.6				
	40	96.0				
	45	107.3				
	50	110.1				
	55	105.2				
	60	117.7				

RESULTS	THC (ppmwv as CH4)	NOx (ppmdv)	CO (ppmdv)	O2 (%)	CO2 (%)
TEST AVERAGE	95.5	24.4	164.4	17.0	3.7
BIAS CORRECTED	94.9	23.7	158.4	17.1	3.6
FLOWRATE (dscfm)	30,687				
FLOWRATE (scfm)	39,100				
lbs/hr	9.25	5.21	21.21		

EML  
CEM SHEET

SOURCE:	Louisiana-Pacific Corp.	TEST:	3
DATE:	7/9/96	COLLECTED	
METHOD:	3A, 7E, 10, & 25A	BY:	ED
UNIT:	Thermal Oxidizer Inlet Site 1	WITNESSED	
FUEL:	Propane	BY:	N/A
LOAD:	N/A		

STEP	DESCRIPTION	LIMIT	THC	NOx	CO	O2	CO2
1	RANGE		1000	250	1000	25.0	25.0
2	CAL GAS						
	ZERO		0	0	0	0	0
	LOW		283				
	MID (bias cal. gas)		513	99	498	12.80	12.60
	SPAN		901	241	883	22.6	19.7
3	INT. LOCAL CAL		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		1.8	0.2	3.3	0.1	-0.1
	% ERROR	±2 (±5% for THC)	0.2%	0.1%	0.3%	0.4%	-0.4%
	LOW (PPM OR %)		284.0				
	% ERROR	±2 (±5% for THC)	0.1%				
	MID (PPM OR %)		512.5	97.5	512.5	13.0	12.7
	% ERROR	±2 (±5% for THC)	-0.1%	-0.6%	1.5%	0.8%	0.4%
	HIGH (PPM OR %)		908.9	242.7	882.9	22.5	19.6
	% ERROR	±2 (±5% for THC)	0.8%	0.7%	0.0%	-0.4%	-0.4%
4	INT. BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO		11.3	0.4	2.3	0.2	0.1
	CAL BIAS	±5%	1.0%	0.1%	-0.1%	0.4%	0.8%
	UPSCALE		285.6	99.2	509.8	12.8	12.6
	CAL BIAS	±5%	0.2%	0.7%	-0.3%	-0.8%	-0.4%
5	RESP. TIME (SEC)		30.0	30.0	15.0	15.0	10.0
6	FINAL BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		8.7	0.9	1.9	0.1	0.0
	DRIFT	±3%	-0.3%	0.2%	0.0%	-0.4%	-0.4%
	CAL BIAS	±5%	0.7%	0.3%	-0.1%	0.0%	0.4%
	UPSCALE (MID) (PPM OR %)		285.5	100.5	513.0	12.8	12.7
	DRIFT	±3%	0.0%	0.5%	0.3%	0.0%	0.4%
	CAL BIAS	±5%	0.2%	1.2%	0.1%	-0.8%	0.0%
7	AVG SYSTEM BIAS		THC	NOx	CO	O2	CO2
	ZERO		10.0	0.7	2.1	0.2	0.1
	UPSCALE		285.6	99.9	511.4	12.8	12.7
Test 3	Integrated Avg		THC	NOx	CO	O2	CO2
1955-2055							
	5		99.7	18.9	168.9	17.2	3.5
	10		86.7	19.2	180.5	17.1	3.6
	15		88.3	21.1	141.7	17.4	3.4
	20		103.1	20.1	189.9	17.1	3.7
	25		101.3	19.7	194.1	17.0	3.8
	30		111.8				
	35		110.3				
	40		121.4				
	45		112.4				
	50		121.5				
	55		134.4				
	60		103.1				

RESULTS	THC (ppmwv as CH4)	NOx (ppmdv)	CO (ppmdv)	O2 (%)	CO2 (%)
TEST AVERAGE	107.8	19.8	175.0	17.2	3.6
BIAS CORRECTED	107.0	19.1	169.1	17.2	3.6
FLOWRATE (dscfm)	32,465				
FLOWRATE (scfm)	40,844				
lbs/hr	10.89	4.45	23.95		

EML  
CEM SHEET

SOURCE:	Louisiana-Pacific Corp.	TEST:	1
DATE:	7/9/96	COLLECTED	
METHOD:	3A, 7E, 10, & 25A	BY:	ED
UNIT:	Thermal Oxidizer Inlet Site 2	WITNESSED	
FUEL:	Propane	BY:	N/A
LOAD:	N/A		

STEP	DESCRIPTION	LIMIT	THC	NOx	CO	O2	CO2
1	RANGE		1000	250	1000	25.0	25.0
2	CAL GAS						
	ZERO		0	0	0	0	0
	LOW		283				
	MID (bias cal. gas)		513	99	498	12.80	12.60
	SPAN		901	241	883	22.6	19.7
3	INT. LOCAL CAL		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		6.2	0.2	3.3	0.1	-0.1
	% ERROR	±2 (±5% for THC)	0.6%	0.1%	0.3%	0.4%	-0.4%
	LOW (PPM OR %)		291.0				
	% ERROR	±2 (±5% for THC)	0.8%				
	MID (PPM OR %)		523.3	97.5	512.5	13.0	12.7
	% ERROR	±2 (±5% for THC)	1.0%	-0.6%	1.5%	0.8%	0.4%
	HIGH (PPM OR %)		906.9	242.7	882.9	22.5	19.6
	% ERROR	±2 (±5% for THC)	0.6%	0.7%	0.0%	-0.4%	-0.4%
4	INT. BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO		6.2	1.3	3.1	0.1	0.1
	CAL BIAS	±5%	0.0%	0.4%	0.0%	0.0%	0.8%
	UPSCALE		291.0	97.6	512.3	12.7	12.5
	CAL BIAS	±5%	0.0%	0.0%	0.0%	-1.2%	-0.8%
5	RESP. TIME (SEC)		30.0	30.0	15.0	15.0	10.0
6	FINAL BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		8.6	1.0	3.7	0.1	0.0
	DRIFT	±3%	0.2%	-0.1%	0.1%	0.0%	-0.4%
	CAL BIAS	±5%	0.2%	0.3%	0.0%	0.0%	0.4%
	UPSCALE (MID) (PPM OR %)		289.0	100.8	510.6	12.8	12.6
	DRIFT	±3%	-0.2%	1.3%	-0.2%	0.4%	0.4%
	CAL BIAS	±5%	-0.2%	1.3%	-0.2%	-0.8%	-0.4%
7	AVG SYSTEM BIAS		THC	NOx	CO	O2	CO2
	ZERO		7.4	1.2	3.4	0.1	0.1
	UPSCALE		290.0	99.2	511.5	12.8	12.6

Test 1	Integrated Avg	THC	NOx	CO	O2	CO2
1515-1615						
	5	149.3				
	10	145.7				
	15	194.6				
	20	174.3				
	25	209.2				
	30	209.7				
	35	196.6	15.8	1046.3	17.2	3.5
	40	215.4	17.8	389.2	17.2	3.5
	45	193.8	17.7	490.5	17.1	3.6
	50	178.3	16.5	418.0	17.2	3.4
	55	171.6	15.5	380.2	17.3	3.3
	60	173.4	16.3	363.1	17.4	3.3

RESULTS	THC (ppmwv as CH4)	NOx (ppmdv)	CO (ppmdv)	O2 (%)	CO2 (%)
TEST AVERAGE	184.3	16.6	514.6	17.2	3.4
BIAS CORRECTED	184.9	15.6	501.0	17.3	3.4
FLOWRATE (dscfm)	25,865				
FLOWRATE (scfm)	33,751				
lbs/hr	15.56	2.89	56.54		

EML  
CEM SHEET

SOURCE:	Louisiana-Pacific Corp.	TEST:	2
DATE:	7/9/96	COLLECTED	
METHOD:	3A, 7E, 10, & 25A	BY:	ED
UNIT:	Thermal Oxidizer Inlet Site 2	WITNESSED	
FUEL:	Propane	BY:	N/A
LOAD:	N/A		

STEP	DESCRIPTION	LIMIT	THC	NOx	CO	O2	CO2
1	RANGE		1000	250	1000	25.0	25.0
2	CAL GAS						
	ZERO		0	0	0	0	0
	LOW		283				
	MID	(bias cal. gas)	513	99	498	12.80	12.60
	SPAN		901	241	883	22.6	19.7
3	INT. LOCAL CAL		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		6.2	0.2	3.3	0.1	-0.1
	% ERROR	±2 (±5% for THC)	0.6%	0.1%	0.3%	0.4%	-0.4%
	LOW (PPM OR %)		291.0				
	% ERROR	±2 (±5% for THC)	0.8%				
	MID (PPM OR %)		523.3	97.5	512.5	13.0	12.7
	% ERROR	±2 (±5% for THC)	1.0%	-0.6%	1.5%	0.8%	0.4%
	HIGH (PPM OR %)		906.9	242.7	882.9	22.5	19.6
	% ERROR	±2 (±5% for THC)	0.6%	0.7%	0.0%	-0.4%	-0.4%
4	INT. BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO		8.6	1.0	3.7	0.1	0.0
	CAL BIAS	±5%	0.2%	0.3%	0.0%	0.0%	0.4%
	UPSCALE		289.0	100.8	510.6	12.8	12.6
	CAL BIAS	±5%	-0.2%	1.3%	-0.2%	-0.8%	-0.4%
5	RESP. TIME (SEC)		30.0	30.0	15.0	15.0	10.0
6	FINAL BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		3.1	1.0	1.6	0.1	-0.1
	DRIFT	±3%	-0.6%	0.0%	-0.2%	0.0%	-0.4%
	CAL BIAS	±5%	-0.3%	0.3%	-0.2%	0.0%	0.0%
	UPSCALE (MID) (PPM OR %)		285.0	100.4	507.8	12.8	12.5
	DRIFT	±3%	-0.4%	-0.2%	-0.3%	0.0%	-0.4%
	CAL BIAS	±5%	-0.6%	1.2%	-0.5%	-0.8%	-0.8%
7	AVG SYSTEM BIAS		THC	NOx	CO	O2	CO2
	ZERO		5.9	1.0	2.7	0.1	-0.1
	UPSCALE		287.0	100.6	509.2	12.8	12.6

Test 2	Integrated Avg	THC	NOx	CO	O2	CO2
1730-1900						
1735	5	117.1				
1740	10	125.4				
1745	15	168.9				
1820	20	184.4				
	25	157.6				
	30	147.1	15.6	208.9	17.7	3.0
	35	180.3	16.3	416.3	17.2	3.5
	40	180.3	16.7	421.8	17.2	3.5
	45	153.9	15.9	342.7	17.4	3.3
	50	161.5	15.8	373.7	17.3	3.4
	55	138.3	15.9	312.6	17.5	3.2
1900	60	143.5	15.9	329.3	17.4	3.2

RESULTS	THC (ppmw as CH4)	NOx (ppmdv)	CO (ppmdv)	O2 (%)	CO2 (%)
TEST AVERAGE	154.9	16.0	343.6	17.4	3.3
BIAS CORRECTED	152.9	14.9	335.2	17.4	3.4
FLOWRATE (dscfm)	25,862				
FLOWRATE (scfm)	34,488				
lbs/hr	13.15	2.77	37.82		

EML  
CEM SHEET

SOURCE:	Louisiana-Pacific Corp.	TEST:	3
DATE:	7/9/96	COLLECTED	
METHOD:	3A, 7E, 10, & 25A	BY:	ED
UNIT:	Thermal Oxidizer Inlet Site 2	WITNESSED	
FUEL:	Propane	BY:	N/A
LOAD:	N/A		

STEP	DESCRIPTION	LIMIT	THC	NOx	CO	O2	CO2
1	RANGE		1000	250	1000	25.0	25.0
2	CAL GAS						
	ZERO		0	0	0	0	0
	LOW		283				
	MID (bias cal. gas)		513	99	498	12.80	12.60
	SPAN		901	241	883	22.6	19.7
3	INT. LOCAL CAL		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		6.2	0.2	3.3	0.1	-0.1
	% ERROR	±2 (±5% for THC)	0.6%	0.1%	0.3%	0.4%	-0.4%
	LOW (PPM OR %)		291.0				
	% ERROR	±2 (±5% for THC)	0.8%				
	MID (PPM OR %)		523.3	97.5	512.5	13.0	12.7
	% ERROR	±2 (±5% for THC)	1.0%	-0.6%	1.5%	0.8%	0.4%
	HIGH (PPM OR %)		906.9	242.7	882.9	22.5	19.6
	% ERROR	±2 (±5% for THC)	0.6%	0.7%	0.0%	-0.4%	-0.4%
4	INT. BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO		3.1	1.0	1.6	0.1	-0.1
	CAL BIAS	±5%	-0.3%	0.3%	-0.2%	0.0%	0.0%
	UPSCALE		285.0	100.4	507.8	12.8	12.5
	CAL BIAS	±5%	-0.6%	1.2%	-0.5%	-0.8%	-0.8%
5	RESP. TIME (SEC)		30.0	30.0	15.0	15.0	10.0
6	FINAL BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		3.1	1.0	1.6	0.1	-0.1
	DRIFT	±3%	0.0%	0.0%	0.0%	0.0%	0.0%
	CAL BIAS	±5%	-0.3%	0.3%	-0.2%	0.0%	0.0%
	UPSCALE (MID) (PPM OR %)		285.0	100.4	507.8	12.8	12.5
	DRIFT	±3%	0.0%	0.0%	0.0%	0.0%	0.0%
	CAL BIAS	±5%	-0.6%	1.2%	-0.5%	-0.8%	-0.8%
7	AVG SYSTEM BIAS		THC	NOx	CO	O2	CO2
	ZERO		3.1	1.0	1.6	0.1	-0.1
	UPSCALE		285.0	100.4	507.8	12.8	12.5

Test 3	Integrated Avg	THC	NOx	CO	O2	CO2
1955-2055						
	5	176.9				
	10	191.8				
	15	214.8				
	20	191.4				
	25	178.8				
	30	180.9				
	35	189.5	16.4	216.9	17.7	3.1
	40	194.4	15.2	411.5	17.3	3.4
	45	180.1	15.2	376.0	17.4	3.3
	50	199.7	15.4	483.4	17.3	3.4
	55	213.1	15.6	520.8	17.1	3.6
	60	214.6	15.9	516.0	17.0	3.7

RESULTS	THC (ppmwv as CH4)	NOx (ppmdv)	CO (ppmdv)	O2 (%)	CO2 (%)
TEST AVERAGE	193.8	15.6	420.8	17.3	3.4
BIAS CORRECTED	192.1	14.6	412.4	17.3	3.5
FLOWRATE (dscfm)	25,314				
FLOWRATE (scfm)	34,464				
lbs/hr	16.50	2.64	45.54		

EML  
CEM SHEET

SOURCE:	Louisiana-Pacific Corp.	TEST:	1
DATE:	7/9/96	COLLECTED	
METHOD:	3A, 7E, 10, & 25A	BY:	BH
UNIT:	Site #4	WITNESSED	
FUEL:	Propane	BY:	N/A
LOAD:	N/A		

STEP	DESCRIPTION	LIMIT	THC	NOx	CO	O2	CO2
1	RANGE		100	250	1000	25.0	25.0
2	CAL GAS						
	ZERO		0	0	0	0	0
	LOW		16				
	MID	(bias cal. gas)	49	120	498	12.40	12.30
	SPAN		101	237	884	22.1	19.9
3	INT. LOCAL CAL		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		0.0	0.0	-1.1	0.3	0.3
	% ERROR	±2 (±5% for THC)	0.0%	0.0%	-0.1%	1.2%	1.2%
	LOW (PPM OR %)		14.7				
	% ERROR	±2 (±5% for THC)	-1.6%				
	MID (PPM OR %)		51.3	124.6	514.8	12.7	12.7
	% ERROR	±2 (±5% for THC)	2.4%	1.8%	1.7%	1.2%	1.6%
	HIGH (PPM OR %)		97.0	240.6	872.1	22.0	19.9
	% ERROR	±2 (±5% for THC)	-4.0%	1.4%	-1.2%	-0.4%	0.0%
4	INT. BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO		0.0	-0.8	-0.6	0.3	0.3
	CAL BIAS	±5%	0.0%	-0.3%	0.1%	0.0%	0.0%
	UPSCALE		14.7	123.3	492.0	12.7	12.7
	CAL BIAS	±5%	0.0%	-0.5%	-2.3%	0.0%	0.0%
5	RESP. TIME (SEC)		30.0	30.0	30.0	15.0	20.0
6	FINAL BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		0.0	0.4	16.3	0.1	0.3
	DRIFT	±3%	0.0%	0.5%	1.7%	-0.8%	0.0%
	CAL BIAS	±5%	0.0%	0.2%	1.7%	-0.8%	0.0%
	UPSCALE (MID) (PPM OR %)		17.6	116.2	470.6	12.5	12.0
	DRIFT	±3%	2.9%	-2.8%	-2.1%	-0.8%	-2.8%
	CAL BIAS	±5%	2.9%	-3.4%	-4.4%	-0.8%	-2.8%
7	AVG SYSTEM BIAS		THC	NOx	CO	O2	CO2
	ZERO		0.0	-0.2	7.9	0.2	0.3
	UPSCALE		16.2	119.8	481.3	12.6	12.4

Test 1	Integrated Avg	THC	NOx	CO	O2	CO2
1515-1615						
	5	1.0	16.8	51.7	16.7	3.8
	10	0.4	16.7	46.1	16.6	4.0
	15	0.5	16.6	54.3	16.6	3.9
	20	0.5	16.0	63.7	16.8	3.8
	25	0.8	17.3	60.6	16.7	3.8
	30	0.9	15.8	72.3	16.6	4.0
	35	1.1				
	40	3.4				
	45	3.3				
	50	4.4				
	55	5.1				
	60	15.2				

RESULTS	THC	NOx	CO	O2	CO2
	(ppmwv as CH4)	(ppmdv)	(ppmdv)	(%)	(%)
TEST AVERAGE	3.1	16.5	58.1	16.7	3.9
BIAS CORRECTED	3.3	16.7	52.9	16.5	3.7
FLOWRATE (dscfm)	62553				
FLOWRATE (scfm)	81266				
lbs/hr	0.66	7.50	14.43		

EML  
CEM SHEET

SOURCE:	Louisiana-Pacific Corp.	TEST:	2
DATE:	7/9/96	COLLECTED	
METHOD:	3A, 7E, 10, & 25A	BY:	BH
UNIT:	Site #4	WITNESSED	
FUEL:	Propane	BY:	N/A
LOAD:	N/A		

STEP	DESCRIPTION	LIMIT	THC	NOx	CO	O2	CO2
1	RANGE		100	250	1000	25.0	25.0
2	CAL GAS						
	ZERO		0	0	0	0	0
	LOW		16				
	MID	(bias cal. gas)	49	120	498	12.40	12.30
	SPAN		101	237	884	22.1	19.9
3	INT. LOCAL CAL		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		0.0	0.0	-1.1	0.3	0.3
	% ERROR	±2 (±5% for THC)	0.0%	0.0%	-0.1%	1.2%	1.2%
	LOW (PPM OR %)		14.7				
	% ERROR	±2 (±5% for THC)	-1.6%				
	MID (PPM OR %)		51.3	124.6	514.8	12.7	12.7
	% ERROR	±2 (±5% for THC)	2.4%	1.8%	1.7%	1.2%	1.6%
	HIGH (PPM OR %)		97.0	240.6	872.1	22.0	19.9
	% ERROR	±2 (±5% for THC)	-4.0%	1.4%	-1.2%	-0.4%	0.0%
4	INT. BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO		0.0	-0.8	-0.6	0.3	0.3
	CAL BIAS	±5%	0.0%	-0.3%	0.1%	0.0%	0.0%
	UPSCALE		17.6	116.2	470.6	12.5	12.0
	CAL BIAS	±5%	2.9%	-3.4%	-4.4%	-0.8%	-2.8%
5	RESP. TIME (SEC)		30.0	30.0	30.0	15.0	20.0
6	FINAL BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		0.0	0.3	2.7	0.2	0.2
	DRIFT	±3%	0.0%	0.4%	0.3%	-0.4%	-0.4%
	CAL BIAS	±5%	0.0%	0.1%	0.4%	-0.4%	-0.4%
	UPSCALE (MID) (PPM OR %)		17.0	116.7	485.8	12.7	11.4
	DRIFT	±3%	-0.6%	0.2%	1.5%	0.8%	-2.4%
	CAL BIAS	±5%	2.3%	-3.2%	-2.9%	0.0%	-5.2%
7	AVG SYSTEM BIAS		THC	NOx	CO	O2	CO2
	ZERO		0.0	-0.3	1.1	0.3	0.3
	UPSCALE		17.3	116.5	478.2	12.6	11.7

Test 2	Integrated Avg	THC	NOx	CO	O2	CO2
1730-1910						
	5	6.2				
	10	7.5				
	15	7.3				
	20	16.9				
	25	18.2				
	30	14.7				
	35	5.6	6.7	31.7	17.1	3.3
	40	0.9	18.2	57.1	16.3	5.9
	45	1.1	17.5	55.1	16.0	6.0
	50	0.8	17.1	59.0	16.0	6.5
	55	1.0	18.0	60.7	16.2	6.5
	60	1.0	15.1	44.4	16.1	6.2

RESULTS	THC (ppmwv as CH4)	NOx (ppmdv)	CO (ppmdv)	O2 (%)	CO2 (%)
TEST AVERAGE	6.8	15.4	51.3	16.3	5.7
BIAS CORRECTED	7.2	16.1	52.5	16.1	5.9
FLOWRATE (dscfm)	63344				
FLOWRATE (scfm)	82031				
lbs/hr	1.48	7.32	14.50		

EML  
CEM SHEET

SOURCE:	Louisiana-Pacific Corp.	TEST:	3
DATE:	7/9/96	COLLECTED	
METHOD:	3A, 7E, 10, & 25A	BY:	BH
UNIT:	Site #4	WITNESSED	
FUEL:	Propane	BY:	N/A
LOAD:	N/A		

STEP	DESCRIPTION	LIMIT	THC	NOx	CO	O2	CO2
1	RANGE		100	250	1000	25.0	25.0
2	CAL GAS						
	ZERO		0	0	0	0	0
	LOW		16				
	MID	(bias cal. gas)	49	120	498	12.40	12.30
	SPAN		101	237	884	22.1	19.9
3	INT. LOCAL CAL		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		0.0	0.0	-1.1	0.3	0.3
	% ERROR	±2 (±5% for THC)	0.0%	0.0%	-0.1%	1.2%	1.2%
	LOW (PPM OR %)		14.7				
	% ERROR	±2 (±5% for THC)	-1.6%				
	MID (PPM OR %)		51.3	124.6	514.8	12.7	12.7
	% ERROR	±2 (±5% for THC)	2.4%	1.8%	1.7%	1.2%	1.6%
	HIGH (PPM OR %)		97.0	240.6	872.1	22.0	19.9
	% ERROR	±2 (±5% for THC)	-4.0%	1.4%	-1.2%	-0.4%	0.0%
4	INT. BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO		0.0	-0.8	-0.6	0.3	0.3
	CAL BIAS	±5%	0.0%	-0.3%	0.1%	0.0%	0.0%
	UPSCALE		17.0	116.7	485.8	12.7	11.4
	CAL BIAS	±5%	2.3%	-3.2%	-2.9%	0.0%	-5.2%
5	RESP. TIME (SEC)		30.0	30.0	30.0	15.0	20.0
6	FINAL BIAS CHECK		THC	NOx	CO	O2	CO2
	ZERO (PPM OR %)		0.0	3.6	3.5	0.3	0.3
	DRIFT	±3%	0.0%	1.8%	0.4%	0.0%	0.0%
	CAL BIAS	±5%	0.0%	1.4%	0.5%	0.0%	0.0%
	UPSCALE (MID) (PPM OR %)		16.3	118.2	479.0	12.6	12.0
	DRIFT	±3%	-0.7%	0.6%	-0.7%	-0.4%	2.4%
	CAL BIAS	±5%	1.6%	-2.6%	-3.6%	-0.4%	-2.8%
7	AVG SYSTEM BIAS		THC	NOx	CO	O2	CO2
	ZERO		0.0	1.4	1.5	0.3	0.3
	UPSCALE		16.7	117.5	482.4	12.7	11.7

Test 3	Integrated Avg	THC	NOx	CO	O2	CO2
1955-2055						
	5	7.3				
	10	7.0				
	15	7.1				
	20	7.1				
	25	7.0				
	30	8.0				
	35	6.9	NA	NA	NA	NA
	40	1.5	15.7	63.1	16.4	5.0
	45	1.3	16.9	63.9	16.1	4.5
	50	1.6	16.8	69.2	16.1	4.6
	55	1.2	15.9	68.0	16.6	4.2
	60	0.8	16.3	42.2	15.6	4.0

RESULTS	THC	NOx	CO	O2	CO2
	(ppmwv as CH4)	(ppmdv)	(ppmdv)	(%)	(%)
TEST AVERAGE	4.7	16.3	61.3	16.2	4.5
BIAS CORRECTED	3.4	15.4	62.0	15.9	4.5
FLOWRATE (dscfm)	62173				
FLOWRATE (scfm)	80984				
lbs/hr	0.70	6.87	16.80		

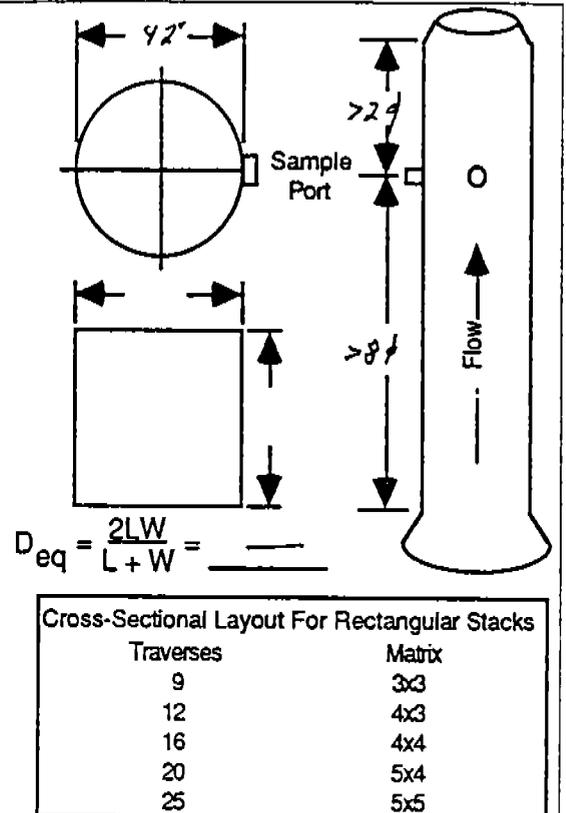
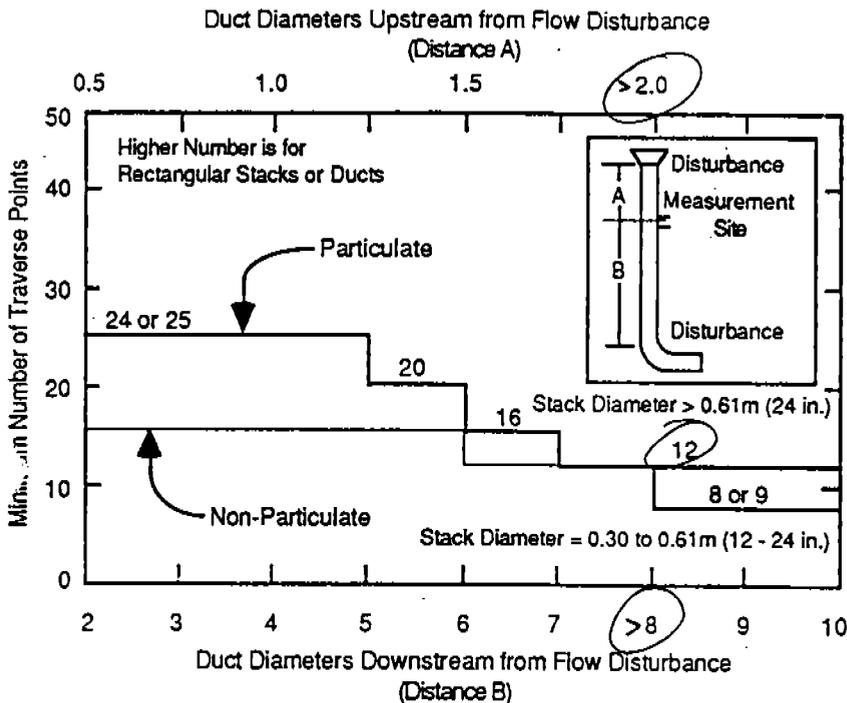
**APPENDIX C**

**Field Data**

Firm LOUISIANA PACIFIC CORP  
 Date 9 JULY 96 Project No. 96053  
 Location #1  
 Diameters Upstream > 24  
 Diameters Downstream 78

Total Traverse Points Required 12  
 Number of Ports 2  
 Points Per Port 6  
 Probe Traverses: Horizontal X  
 Vertical X

**MINIMUM NUMBER OF TRAVERSE POINTS FOR PARTICULATE AND NON-PARTICULATE TRAVERSES**

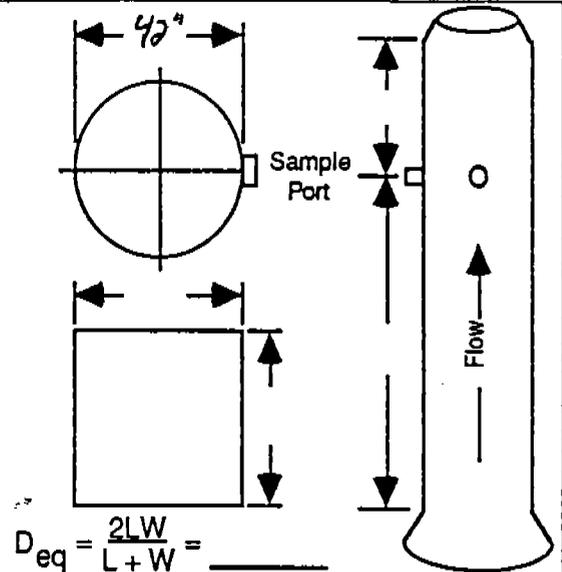
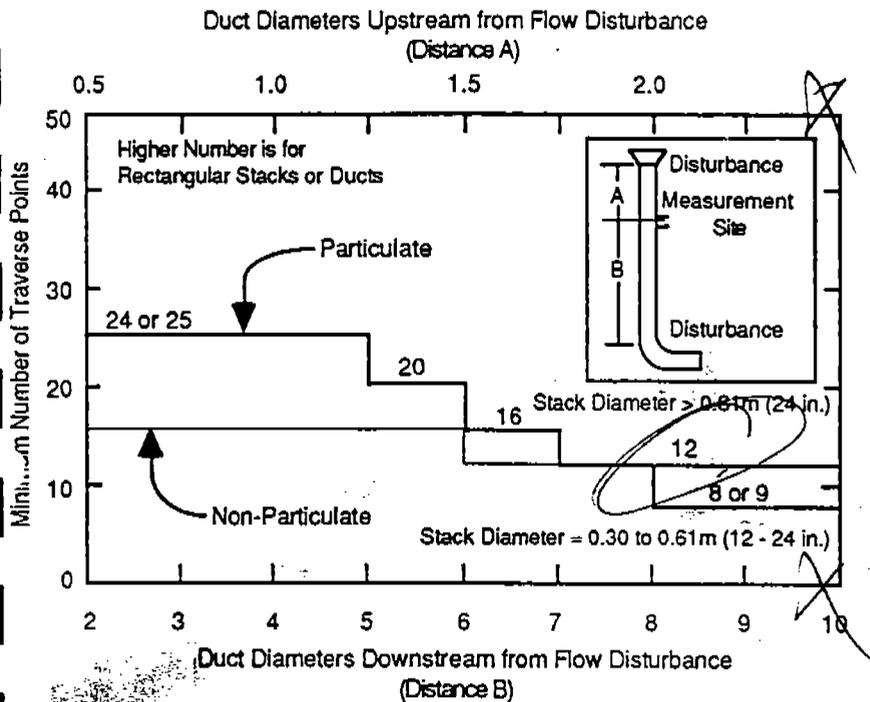


Point On A Diameter	Location of Traverse Points in Circular Stacks*					Traverse Point Location		
	Number of Traverse Points on a Diameter					Distance From Wall	Nipple Size	Total Distance
	4	6	8	10	12			
1	6.7	4.4	3.2	2.6	2.1	1.85	6"	7.9
2	25.0	14.6	10.5	8.2	6.7	6.13		12.1
3	75.0	29.6	19.4	14.6	11.8	12.43		18.4
4	93.3	70.4	32.3	22.6	17.7	29.57		35.6
5		85.4	67.7	34.2	25.0	35.87		41.9
6		95.6	80.6	65.8	35.6	40.15		46.2
7			89.5	77.4	64.4			
8			96.8	85.4	75.0			
9				91.8	82.3			
10				97.4	88.2			
11					93.3			
12					97.9			

\*Percent of Stack Diameter from Inside Wall to Traverse Point

Firm LOUISIANA - PACIFIC Total Traverse Points Required 12  
 Date 7/9/96 Project No. 96053 Number of Ports 2  
 Location #2 Points Per Port 6  
 Diameters Upstream 3" Probe Traverses: Horizontal YES 10#3  
 Diameters Downstream 10" Vertical YES 10#2

**MINIMUM NUMBER OF TRAVERSE POINTS FOR PARTICULATE AND NON-PARTICULATE TRAVERSES**



**Cross-Sectional Layout For Rectangular Stacks**

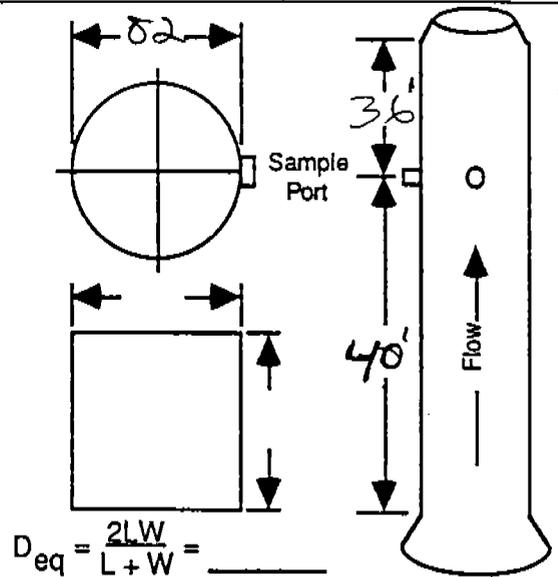
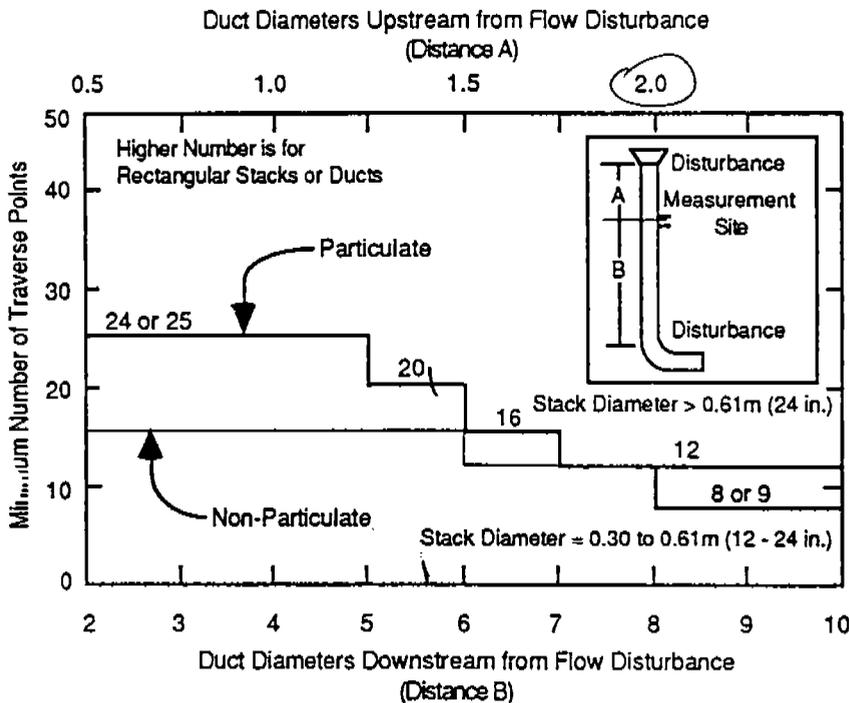
Traverses	Matrix
9	3x3
12	4x3
16	4x4
20	5x4
25	5x5

Point On A Diameter	Location of Traverse Points in Circular Stacks*					Traverse Point Location		
	Number of Traverse Points on a Diameter					Distance From Wall	Nipple Size	Total Distance
	4	6	8	10	12			
1	6.7	4.4	3.2	2.6	2.1	1.85	6"	7.9
2	25.0	14.6	10.5	8.2	6.7	6.13		12.1
3	75.0	29.6	19.4	14.6	11.8	12.43		18.4
4	93.3	70.4	32.3	22.6	17.7	29.57		35.6
5		85.4	67.7	34.2	25.0	35.87		41.9
6		95.6	80.6	65.8	35.6	40.15		46.2
7			89.5	77.4	64.4			
8			96.8	85.4	75.0			
9				91.8	82.3			
10				97.4	88.2			
11					93.3			
12					97.9			

\*Percent of Stack Diameter from Inside Wall to Traverse Point

Firm LP Total Traverse Points Required 20  
 Date 7-9-96 Project No. 96053 Number of Ports 2  
 Location STACK Points Per Port 10  
 Diameters Upstream 5.85 Probe Traverses: Horizontal   
 Diameters Downstream 5.27 Vertical

**MINIMUM NUMBER OF TRAVERSE POINTS FOR PARTICULATE AND NON-PARTICULATE TRAVERSES**



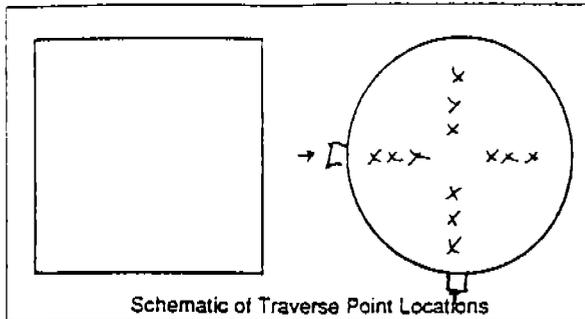
**Cross-Sectional Layout For Rectangular Stacks**

Traverses	Matrix
9	3x3
12	4x3
16	4x4
20	5x4
25	5x5

Point On A Diameter	Location of Traverse Points in Circular Stacks*					Traverse Point Location		
	Number of Traverse Points on a Diameter					Distance From Wall	Nipple Size	Total Distance
	4	6	8	10	12			
1	6.7	4.4	3.2	2.6	2.1	2.13	6	8.13
2	25.0	14.6	10.5	8.2	6.7	6.7		12.7
3	75.0	29.6	19.4	14.6	11.8	11.9		17.9
4	93.3	70.4	32.3	22.6	17.7	18.5		24.5
5		85.4	67.7	34.2	25.0	28		34
6		95.6	80.6	65.8	35.6	54		60
7			89.5	77.4	64.4	63.5		69.5
8			96.8	85.4	75.0	70		76
9				91.8	82.3	75.3		81.3
10				97.4	88.2	79.8		85.8
11					93.3			
12					97.9			

\*Percent of Stack Diameter from Inside Wall to Traverse Point

Firm LOUISIANA PACIFIC CORP  
 Date 9 JULY 76 Project No. 96053  
 Location INLET #1  
 Round Stack or Duct:  
 Diameter (in) 42" Area 9.62 ft<sup>2</sup>  
 Rectangular Stack or Duct:  
 Stack Length (in) - Area - ft<sup>2</sup>  
 Stack Width (in) -  
 Barometric Pressure; Pb = 29.95 in. Hg  
 Stack Static Pressure; Pg = -10.2" H<sub>2</sub>O in. Hg  
 Stack Gas Moisture Content; % H<sub>2</sub>O = 20%  
 Stack Gas Molecular Weight; (wet) Mw = 28  
 Pitot Tube No. 601 Cp = 0.84  
 Field Tester(s) MM PO  
 Test Start Time: 0945 Finish: 0950



Cyclonic Flow Angle: + ⓪ Clockwise  
 - ⓪ Counterwise

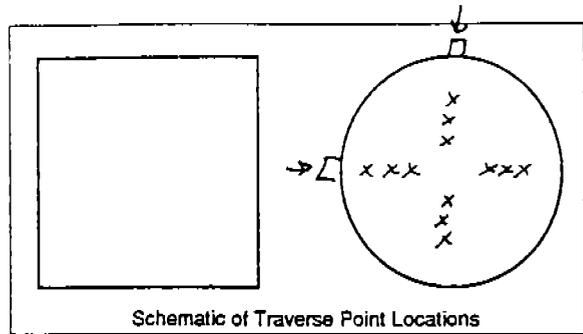
0.221 CALC NOZZLE 0.244 ACTUAL NOZZLE

PORT	POINT	ΔP (Inch H <sub>2</sub> O)	√ΔP	Ts (°F)	± ⓪	Pitots Reversed for Negative Flow?	RADIANS	√ΔP*cos⓪
1(V)	1	1.8	1.342	220	0°	-	0	
	2	1.7	1.304	219		-		
	3	1.7	1.304	220		-		
	4	1.7	1.304	219		-		
	5	1.7	1.304	219		-		
	6	1.8	1.342	220		-		
2(H)	1	1.6	1.265	220	↓	-	↓	
	2	1.9	1.378	220		-		
	3	1.8	1.342	219		-		
	4	1.7	1.304	220		-		
	5	1.6	1.265	221		-		
	6	0.99	0.995	207		-		
AVG		1.666						
AVERAGE			1.287	218.7			AVERAGE	

Absolute Gas Temperature; Tst = Ts + 460°  
 Absolute Gas Pressure; Ps = Pb + Pg/13.6  
 Gas Velocity; Vs = (85.49)Cp(√ΔP\*cos⓪)avg√(Tst avg/(Ps\*Mw))  
 Actual Gas Flow Rate; Qa = (Vs)(60)(A)  
 Standard Gas Flow Rate; Qsw = Qa(528°R/Tst)(Ps/29.92)  
 Dry Standard Gas Flow Rate; Qsd = Qa(528°R/Tst)(Ps/29.92)((100-%H<sub>2</sub>O)/100)

678.7 °R  
 29.2 In. Hg  
~~34.206~~ ft/sec 8304  
~~48,600~~ acfm 47,908  
~~36,900~~ scfm 36,573  
~~27,520~~ dscfm 27,520  
 29,098 ~~PM~~ with 0.20  
 Page 1 of 2

Firm LOUISIANA PACIFIC CORP.  
 Date 1 JULY 96 Project No. 96053  
 Location INLET #2  
 Round Stack or Duct:  
 Diameter (in) 92" Area 9.62 ft<sup>2</sup>  
 Rectangular Stack or Duct:  
 Stack Length (in) - Area - ft<sup>2</sup>  
 Stack Width (in) -  
 Barometric Pressure; Pb = 29.95 in. Hg  
 Stack Static Pressure; Pg = -8" H<sub>2</sub>O in. Hg  
 Stack Gas Moisture Content; % H<sub>2</sub>O = 20% (ASSUMED)  
 Stack Gas Molecular Weight; (wet) Mw = -  
 Pitot Tube No. 901 Cp = 0.84  
 Field Tester(s) MM TC PO  
 Test Start Time: 0930 Finish: 0939



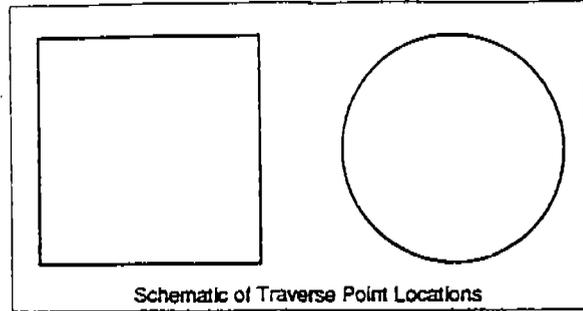
Cyclonic Flow Angle: + Ø Clockwise  
 - Ø Counterwise

PORT	POINT	ΔP (Inch H <sub>2</sub> O)	√ΔP	Ts (°F)	± Ø	Pitots Reversed for Negative Flow?	RADIANS	√ΔP*cosØ
1 (H)	1	1.2	1.095	251	0°	-	0	
	2	1.5	1.225	252				
	3	1.6	1.265	251				
	4	1.5	1.225	250				
	5	1.4	1.183	248				
	6	1.1	1.049	240				
2 (V)	1	1.2	1.095	240	↓	-	↓	
	2	1.4	1.183	247				
	3	1.5	1.225	250				
	4	1.6	1.265	249				
	5	1.5	1.225	247				
	6	1.1	1.049	243				
		<u>1.383</u>						
AVERAGE			<u>1.072</u>	<u>247.3</u>			AVERAGE	

Absolute Gas Temperature; Tst = Ts + 460°  
 Absolute Gas Pressure; Ps = Pb + Pg/13.6  
 Gas Velocity; Vs = (85.49)Cp(√ΔP\*cosØ)avg√(Tst avg/(Ps\*Mw))  
 Actual Gas Flow Rate; Qa = (Vs)(60)(A)  
 Standard Gas Flow Rate; Qs = Qa(528°R/Tst)(Ps/29.92)  
 Dry Standard Gas Flow Rate; Qsd = Qa(528°R/Tst)(Ps/29.92)((100-%H<sub>2</sub>O)/100)

707.3 °R  
29.36 in. Hg  
~~71.40~~ ft/sec 77.09  
~~41,214~~ acfm 44,966  
~~30,130~~ scfm 32,589  
~~24,150~~ dscfm 26,071

Firm LOUISIANA PACIFIC  
 Date 9 JULY 96 Project No. 96053  
 Location JACK  
 Round Stack or Duct:  
 Diameter (in) 82" Area \_\_\_\_\_ ft<sup>2</sup>  
 Rectangular Stack or Duct:  
 Stack Length (in) \_\_\_\_\_ Area \_\_\_\_\_ ft<sup>2</sup>  
 Stack Width (in) \_\_\_\_\_  
 Barometric Pressure; Pb = 29.92 in. Hg  
 Stack Static Pressure; Pg = -.26 in. H2O  
 Stack Gas Moisture Content; % H2O = 20 (Assumed)  
 Stack Gas Molecular Weight; (wet) Mw = 28 (Assumed)  
 Pitot Tube No. 902 Cp = 0.84  
 Field Tester(s) MA AK OT  
 Test Start Time: 11:5 Finish: 11:30



Cyclonic Flow Angle: + Ø Clockwise  
 - Ø Counterwise

CALC NOSE .273 ACTUAL .275

PORT	POINT	ΔP (Inch H2O)	√ΔP	Ts (°F)	± Ø	Pitots Reversed for Negative Flow?	RADIANS	√ΔP*cosØ
	1	.58	0.762	257				
	2	.63	0.794	258				
	3	.63	0.794	260				
	4	.64	0.8	261				
	5	.63	0.794	262				
	6	.58	0.762	254				
	7	.61	0.781	255				
	8	.61	0.781	257				
	9	.59	0.768	259				
	10	.50	0.707	259				
	1	.57	0.755	258				
	2	.57	0.755	255				
	3	.61	0.781	254				
	4	.60	0.775	252				
	5	.61	0.781	253				
	6	.59	0.768	254				
	7	.59	0.768	255				
	8	.58	0.762	257				
	9	.57	0.755	261				
	10	.52	0.721	259				
		.56						
AVERAGE			0.768	257			AVERAGE	

Absolute Gas Temperature; Tst = Ts + 460°  
 Absolute Gas Pressure; Ps = Pb + Pg/13.6  
 Gas Velocity; Vs = (85.49)Cp(√ΔP\*cosØ)avg√(Tst avg/(Ps\*Mw))  
 Actual Gas Flow Rate; Qa = (Vs)(60)(A)  
 Standard Gas Flow Rate; Qs = Qa(528°R/Tst)(Ps/29.92)  
 Dry Standard Gas Flow Rate; Qsd = Qa(528°R/Tst)(Ps/29.92)((100-%H2O)/100)

66.38

7171 °R  
29.77 in. Hg  
50.99 ft/sec  
112,193 acfm  
82,745 scfm  
66,196 dscfm

Client/Firm LP  
 Location STACK  
 Project No. 16053 Test Number 1  
 Testers Initials DT/DK Test Date 7-9-76 Nozzle Size 2.75  
 Test Time (min) 60 Start Time 1515 Nozzle No. 3.57  
 Min Per Point 3 End Time 1616 C/K Factor 3.57

Assumed Moisture 20 ( $\%$ )  
 Pb = 27.88 (in Hg)  
 Module No. 98  
 $\Delta H@ = 2.03$   
 Cp = 0.84  
 Y = 1.00  
 Probe No. 102  
 Pilot No. 902  
 Filter No. 31968

Signature of Train Operator: Dan Koff  
 Rectangular Stack: Length (in) N/A Width (in) N/A  
 Circular Stack: Diameter (in) 8.5 Area (ft<sup>2</sup>) 36.67  
 Train Leak Checks: Pre-Test 0.0 cfm Post-Test 0.0 cfm  
 Orsat Leak Check: Pre-Test N/A Post-Test N/A  
 Pilot Leak Check: Pre-Test ✓ Post-Test ✓  
 Final Orsat Analysis CO<sub>2</sub> 0.2%

Port	Point	Time (min)	Meter Volume (ft <sup>3</sup> )	$\Delta P$ (in. H <sub>2</sub> O)	$\Delta H$ (in. H <sub>2</sub> O)	Temperatures			Cond Out (°F)	Module Meter		Vacuum (in. Hg)	Comments
						Stack (°F)	Probe (°F)	Hi/Box (°F)		Filter (°F)	In (°F)		
A	1		483.000	.52	1.83	255	246	232		79	78	4	Stale Pressure: In H <sub>2</sub> O
	2		485.6	.57	2.01	256	246	231		81	78	4	
	3		488.0	.59	2.1	255	247	232		84	79	5	
	4		490.0	.60	2.1	253	247	237		85	79	5	
	5		492.3	.60	2.1	259	247	237		86	80	5	
	6		494.6	.57	2.0	259	247	238		86	80	5	
	7		496.9	.57	2.0	256	247	238		86	80	5	
	8		499.1	.56	1.99	253	246	237		87	81	5	
	9		501.4	.55	1.96	258	246	236		86	81	5	
	10		503.6	.53	1.87	260	246	236		86	81	5	
	1		508.0	.53	1.89	252	244	235		85	81	5	
	2		510.1	.57	2.0	253	244	235		85	81	5	
	3		512.2	.59	2.1	253	245	235		86	81	5	
	4		514.3	.60	2.1	260	246	231		86	81	5	
	5		515.2	.58	2.07	255	246	235		80	81	5	
	6		517.1	.58	2.07	262	248	235		80	81	5	
	7		519.4	.57	2.0	260	248	235		80	81	5	
	8		521.6	.57	2.0	255	245	236		80	81	5	
	9		523.2	.57	2.0	262	246	232		80	81	5	
	10		524.9	.57	1.89	259	245	233		80	81	5	

Impinger Number	Impinger Recovery		Total Catch
	Vol or Wt Initial	Final	
1	100	324	324
2	100	134	134
3	0	3	3
4			
Other(s)			
Silica Gel			

Final Reading: 83.5 Average of In & Out Meter Temperatures 20.1  
 Total Volume: 42.16 Avg Square Foot  $\Delta P$  .753  
 Average 2.58

Total Moisture Catch: 29.88 Calculated Moisture Content: 0.0000  
 Rev 995 TMC

**EPA Method 5**

Signature of Train Operator:

Client/Firm: LP  
 Location: STACK  
 Project No.: 4053 Test Number: 2  
 Testers Initials: DRK Test Date: 7-9-76 Nozzle Size: 2.25  
 Test Time (min): 60 Start Time: 1730 Nozzle No.: 3.57  
 Min Per Point: 3 End Time: 1910 C/K Factor: 3.57

Assumed Moisture: 20 (%) (In Hg)  
 Pb = 29.88  
 Module No.: 78 ΔH@ = 2.03  
 Cp = 0.84  
 Y = 1.00  
 Probe No.: 902  
 Pilot No.: 902  
 Filter No.: 31969

Rectangular Stack: Length (in) NA Width (in) NA  
 Circular Stack: Diameter (in) 02 Area (ft<sup>2</sup>) 3.67  
 Train Leak Checks: Pre-Test 0.0 cfm In Hg 10  
 Post-Test 0.0 cfm In Hg NA  
 Orsat Leak Check: Pre-Test ✓ Post-Test ✓  
 Pilot Leak Check: Pre-Test ✓ Post-Test ✓  
 Final Orsat Analysis: CEM 02% CEMCO2%

Port	Point	Time (min)	Meter Volume (ft <sup>3</sup> )	AP (In. H2O)	ΔH (In. H2O)	Temperatures			Vacuum		Comments							
						Stack (°F)	Probe (°F)	Hr Box (°F)	Filter (°F)	Cond Out (°F)		Module Meter In. (°F) Out. (°F)	Static Pressure: In H2O					
A	1	3	527300	.56	1.99	250	245	235		47	78	4	STOP RUN RE-START					
	2	6	529.0	.60	2.14	257	246	238		44	79	5						
	3	9	533.8	.60	2.14	258	247	237		52	81	5						
	4	12	536.2	.62	2.21	254	247	238		56	83	5						
	5	15	538.4	.61	2.18	254	248	237		54	83	6						
	6	18	541.1	.61	2.18	262	247	240		54	83	6						
	7	21	543.4	.57	2.03	260	247	238		45	78	6						
	8	24	545.7	.54	1.93	261	247	240		49	78	6						
	9	27	547.9	.53	1.89	255	246	235		53	79	5						
	10	30	550.0	.48	1.71	252	245	242		54	80	5						
B	1		552.1	.52	1.85	257	246	242		55	80	5						
	2		554.4	.60	2.14	254	246	241		55	81	5						
	3		556.6	.62	2.21	260	247	240		58	82	5						
	4		557.1	.63	2.25	259	248	241		61	82	6						
	5		561.6	.60	2.14	255	248	241		64	83	6						
	6		563.9	.59	2.10	255	248	241		69	84	6						
	7		566.2	.58	2.07	263	248	241		54	84	6						
	8		568.5	.60	2.14	260	247	240		50	84	6						
	9		570.3	.53	1.89	254	247	241		48	84	6						
	10		572.810	.46	1.64	257	246	240		48	83	6						
Average											2.04	257	43.41	76	2.04	80	267	267

Impinger Number	Recovery	Vol or Wt		Total Catch
		Initial	Final	
1	100	335	235	335
2	100	130	30	30
3	0	0	2	2
4				
Other(s)				
Silica Gel				



# EPA Method 5

Particulate Test Data Sheet

Client/Firm: LP Location: STACK Assumed Moisture: 20 (%)  $\Delta H_{2O}$ : 2.03  
 Project No.: 4053 Test Number: 3 Pb: 2.99 (In Hg) Cp: 0.84  
 Testers Initials: DR Test Date: 2-7-76 Nozzle Size: 0.275 Y: 1.00  
 Test Time (min): 30 Start Time: 1950 Nozzle No.: 902 Probe No.: 902  
 Mh Per Point: 3 End Time: 2000 C/K Factor: 3.57 Filler No.: 31970

Signature of Train Operator: Duck

Rectangular Stack: Length (in) NA Width (in) NA  
 Circular Stack: Diameter (in) B2 Area (ft<sup>2</sup>) 2.32  
 Train Leak Checks: Pre-Test 0.0 cfm Post-Test 10 In Hg  
 Orsat Leak Check: Pre-Test NA Post-Test NA  
 Pilot Leak Check: Pre-Test U Post-Test U  
 Final Orsat Analysis CFM 02% CO<sub>2</sub> CO<sub>2</sub>%

Port	Point	Time (min)	Meter Volume (ft <sup>3</sup> )	AP (In. H <sub>2</sub> O)	ΔH (In. H <sub>2</sub> O)	Temperatures			Module Meter		Vacuum (In. Hg)	Comments	
						Stack (°F)	Probe (°F)	Htr Box (°F)	Filter (°F)	Cond Out (°F)			In (°F)
A	1	3	573.000	.55	1.96	253	248	270		46	75	76	Static Pressure: In H <sub>2</sub> O
	2	6	575.3	.57	2.03	258	247	274		48	74	76	
	3	9	577.6	.60	2.14	260	248	257		53	74	75	
	4	12	579.9	.63	2.25	255	249	258		51	75	75	
	5	15	582.2	.61	2.17	255	249	260		49	75	75	
	6	18	584.6	.58	2.07	263	249	261		49	76	74	
	7	21	586.7	.57	2.03	258	249	260		49	77	74	
	8	24	589.3	.56	1.99	255	248	260		48	77	74	
	9	27	591.4	.52	1.85	255	248	260		48	78	74	
	10	30	593.7	.46	1.64	256	247	260		50	78	74	
B	1		20.5	.75		252	245	261		50	77	74	Impinger Recovery
	2		598.0	.52	1.85	252	245	261		50	77	74	
	3		600.5	.57	2.03	253	247	259		49	78	73	
	4		602.5	.59	2.10	260	247	260		48	79	74	
	5		605.2	.58	2.07	254	248	260		50	80	74	
	6		607.3	.54	1.93	254	247	259		51	80	74	
	7		609.8	.57	2.03	263	247	259		52	80	74	
	8		612.0	.58	2.07	261	247	258		53	80	74	
	9		614.3	.58	2.07	261	247	259		53	80	74	
	10		616.4	.55	1.96	254	246	258		53	79	74	
Average of In & Out Meter Temperatures												78	

Final Reading: 48.28 Total Volume: 7.79 Avg Square Root ΔP: 2.00 Average: 256  
 Impinger Recovery: Vol or Wt Initial Final Total Catch  
 1 100 245 245  
 2 100 129 129  
 3  
 4  
 Other(s)  
 Silica Gel

# LABORATORY ANALYSIS REPORT

RECEIVED USE 2 0 1996  
**Environmental Health Laboratory**  
a division of CIGNA Loss Control Services, Inc.  
100 Sebethe Drive, Suite A-5  
Cromwell, CT 06416  
(800) 243-4903  
Cromwell (203) 635-6475



Laboratories in Macon, GA and Cromwell, CT

To: Tony Saltis  
Air Pollution Characterization & Control  
60 Industrial Park Road West  
Tolland, CT 06084

Report No.: 96G1087  
P. O. No.: 2896  
Date Received: 7/12/96  
Date Reported: 7/25/96

Analysis: Determination of Condensable Particulate Emissions from Stationary Sources  
Analytical Method: EPA Method 202

Sample Number	mg Inorganic Condensable Particulate Matter	mg Organic Condensable Particulate Matter	mg Total Condensable Particulate Matter
S1 Run 1	80	48	128
S1 Run 2	59	32	91
S1 Run 3	61	32	93
S3 Run 1	71	34	105
S3 Run 2	19	77	96
S3 Run 3	19	19	38
S4 Run 1	18	74	92
S4 Run 2	11	12	23
S4 Run 3	7.5	15	22

A blank was not provided for the analysis. We recommend that a blank control be submitted with each set of samples so that the sampling media can be checked for possible contamination.

As per the method, all inorganic fractions were checked for the possibility of a positive Ammonium Ion interference. All samples except S4 Run 1 indicated that this interference may exist. Further analysis by ion chromatography would be able to determine the amount of this interference, and samples could be corrected if necessary.

Analyst: David Torzillo and Marjorie Luzzi

Date: 7/25/96

< = Less than





284

APCC CHAIN OF CUSTODY

60 INDUSTRIAL PARK ROAD WEST  
TOLLAND CT, 06084

9661087

203-871-8557

Lowie P

PROJECT NO. 96053

PROJECT NAME Lowie P

PROJECT DESCRIPTION	DATE	TIME	COMPOSITE OR GRAB	ANALYSIS REQUIRED	SAMPLING TRAIN	SAMPLE DESCRIPTION	SPECIAL NOTES	SEND TO:
✓ 54 Run 1m	7/9/96			Method 202		Meth Cl		EHL
✓ 54 Run 1DI						.DI H <sub>2</sub> O		
✓ 54 Run 2m						Meth Cl		
✓ 54 Run 2OT						DI		
✓ 54 Run 3m						meth		
✓ 54 Run 3OT						DI		
Relinquished by: (Signature)				Received by: (Signature)				DATE/TIME
Relinquished by: (Signature)				Received by: (Signature)				DATE/TIME
Relinquished by: (Signature)				Received by: (Signature)				DATE/TIME
Relinquished by: (Signature)				Received by: (Signature)				DATE/TIME

**APPENDIX D**  
**IRM Strip Charts**





THE CH 100

THE CH 100

THE CH 100

THE CH 100

04

\*\*\* LOS GRP 1 \*\*\* UNIT 04

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05 09 02 02-11 PC 02 02-11 PC 02 02-11 PC

\*\*\* STARTS PT 07 58:44 \*\*\* ENDS PT 07 58:44 \*\*\*

PT DATE UNIT D LEEDS PT DATE UNIT D LEEDS PT DATE UNIT D LEEDS

01 09 02 02-11 PC 02 02-11 PC 02 02-11 PC

05 09 02 02-11 PC 02 02-11 PC 02 02-11 PC

PT	DATE	UNIT	D	LEEDS	PT	DATE	UNIT	D	LEEDS	PT	DATE	UNIT	D	LEEDS
01	09	02	02-11	PC	02	02-11	PC	02	02-11	PC	02	02-11	PC	02
05	09	02	02-11	PC	02	02-11	PC	02	02-11	PC	02	02-11	PC	02
*** STARTS PT 07 58:44 *** ENDS PT 07 58:44 ***														
01	09	02	02-11	PC	02	02-11	PC	02	02-11	PC	02	02-11	PC	02
05	09	02	02-11	PC	02	02-11	PC	02	02-11	PC	02	02-11	PC	02



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10/2/54

\*\*\* KESL RNDNG 08:25:04 05 11.1  
 \*\*\* KESL RNDNG 08:25:04 05 11.1

10/2/54

10/2/54

10/2/54

\*\*\* STARTS FT 08 23:23 \*\*\* ENDS FT 08 23:23 \*\*\*  
 FT DATA UNITS ST LEVEND FT DATA UNITS ST LEVEND  
 03 21.6 PPH 100  
 03 21.6 PPH 100

\*\*\* STARTS FT 08 23:54 \*\*\* ENDS FT 08 23:54 \*\*\*  
 FT DATA UNITS ST LEVEND FT DATA UNITS ST LEVEND  
 03 21.6 PPH 100  
 03 21.6 PPH 100

\*\*\* KESL RNDNG 08:25:04 05 11.1  
 \*\*\* KESL RNDNG 08:25:04 05 11.1

\*\*\* KESL RNDNG 08:25:04 05 11.1  
 \*\*\* KESL RNDNG 08:25:04 05 11.1  
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 \*\*\* KESL RNDNG 08:25:04 05 11.1  
 \*\*\* KESL RNDNG 08:25:04 05 11.1

\*\*\* L03 ERP 1 \*\*\* INIT 01 \*\*\* STARTS FT 08 23:54 \*\*\* ENDS FT 08 23:54 \*\*\*  
 FT DATA UNITS ST LEVEND FT DATA UNITS ST LEVEND FT DATA UNITS ST LEVEND  
 02 11.1 PPH 100 03 21.6 PPH 100 04 11.1 PPH 100  
 06 21.6 PPH 100 07 21.6 PPH 100 08 21.6 PPH 100





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 \*\*\* STARTS AT 14:15:20 \*\*\* ENDS AT 14:15:20 \*\*\*  
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 \*\*\* UNIT 01 \*\*\*  
 \*\*\* UNIT 01 \*\*\*

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 10/25/98

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 \*\*\* RESET AVERAGE 14.25 08 24 18.7 PPM  
 \*\*\* RESET AVERAGE 14.25 08 25 149.8 PPM  
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 \*\*\* RESET AVERAGE 14.25 08 24 3.5 PPM

\*\*\* RESET AVERAGE 14.25 08 28 4.6 PPM  
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 \*\*\* RESET AVERAGE 14.25 08 24 18.7 PPM  
 \*\*\* RESET AVERAGE 14.25 08 25 149.8 PPM  
 \*\*\* RESET AVERAGE 14.25 08 22 3.2 PPM  
 \*\*\* RESET AVERAGE 14.25 08 24 3.5 PPM

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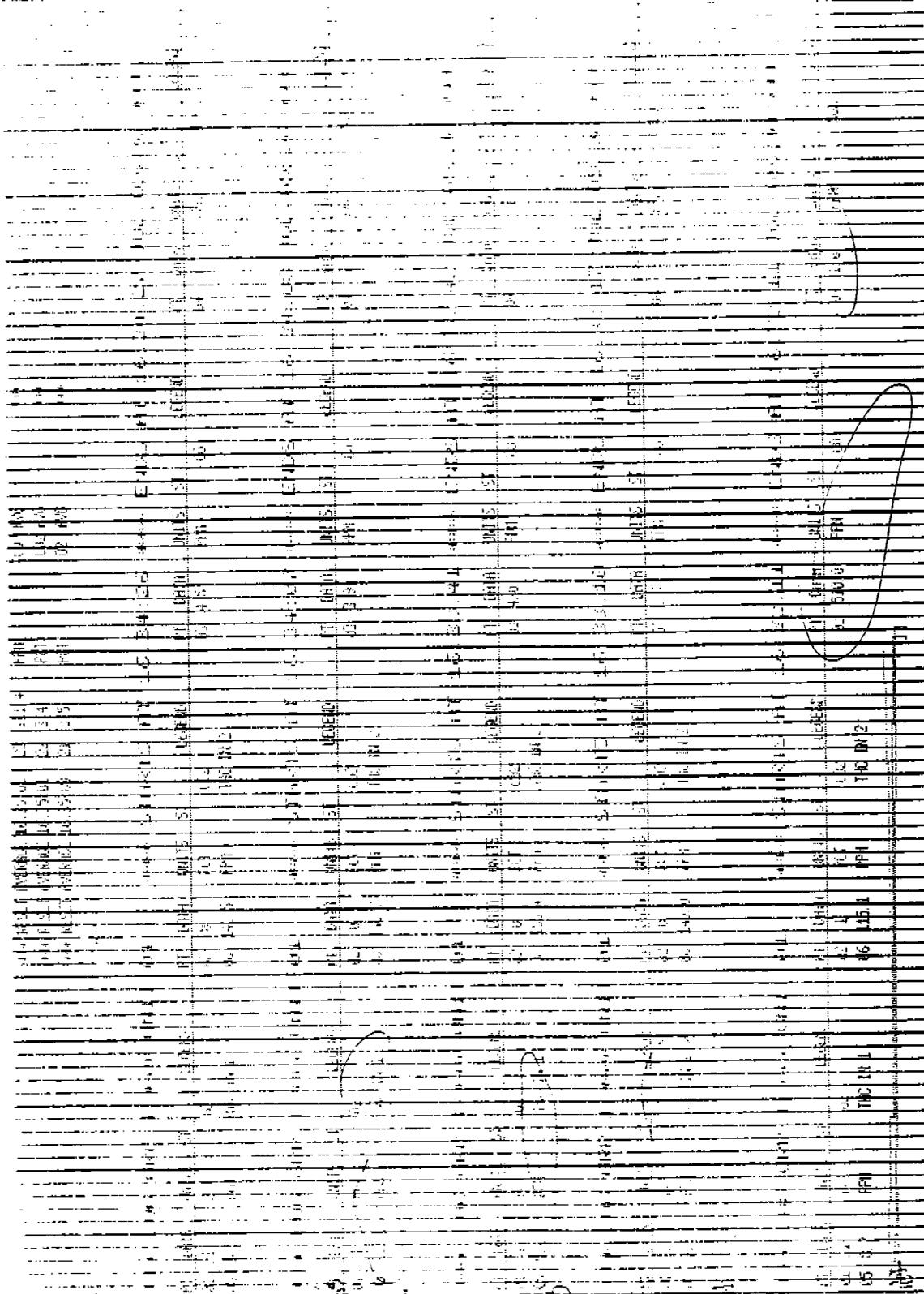
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UNIT 1  
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\*\*\* STARTS AT 16:30:58 \*\*\* ENDS AT 16:39:59 JUL 08 SE \*\*\*

UNIT 1  
 UNIT 2

\*\*\* RESET AVERAGE IN 30.00 24 173.6 PPM  
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\*\*\* RESET AVERAGE 07:40:00 26 115.4 PPM  
 \*\*\* RESET AVERAGE 07:40:00 25 110.0 PPM  
 \*\*\* RESET AVERAGE 07:40:00 24 25.5 PPM  
 \*\*\* RESET AVERAGE 07:40:00 23 216.1 PPM  
 \*\*\* RESET AVERAGE 07:40:00 22 4.1 PPM  
 \*\*\* RESET AVERAGE 07:40:00 21 16.7 PPM

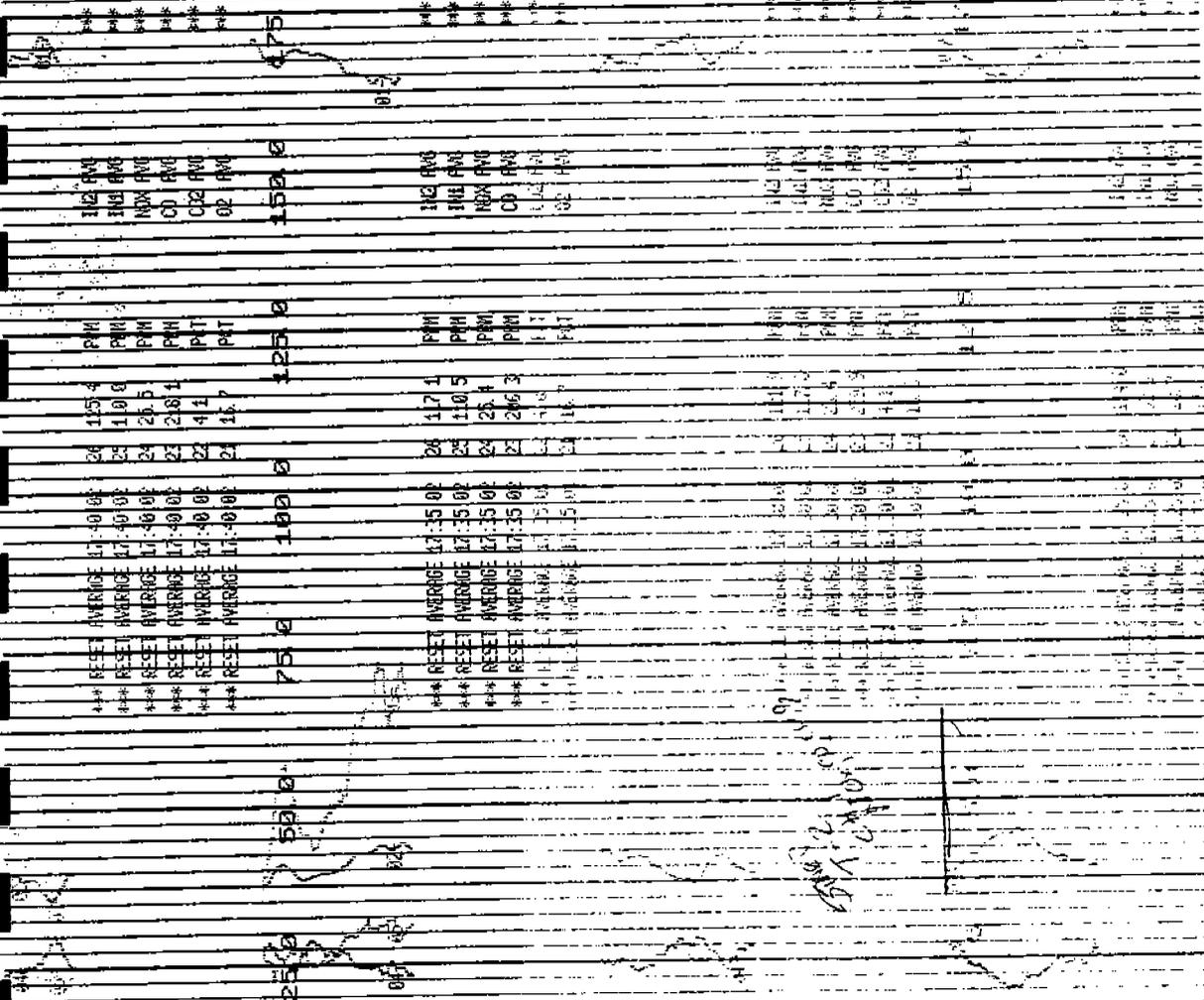
75.0 100.0 125.0 150.0 175.0 200.0 225.0 250.0 PPM

\*\*\* RESET AVERAGE 07:35:00 26 117.1 PPM  
 \*\*\* RESET AVERAGE 07:35:00 25 110.5 PPM  
 \*\*\* RESET AVERAGE 07:35:00 24 25.4 PPM  
 \*\*\* RESET AVERAGE 07:35:00 23 206.3 PPM

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 \*\*\* RESET AVERAGE 07:30:00 24 25.4 PPM  
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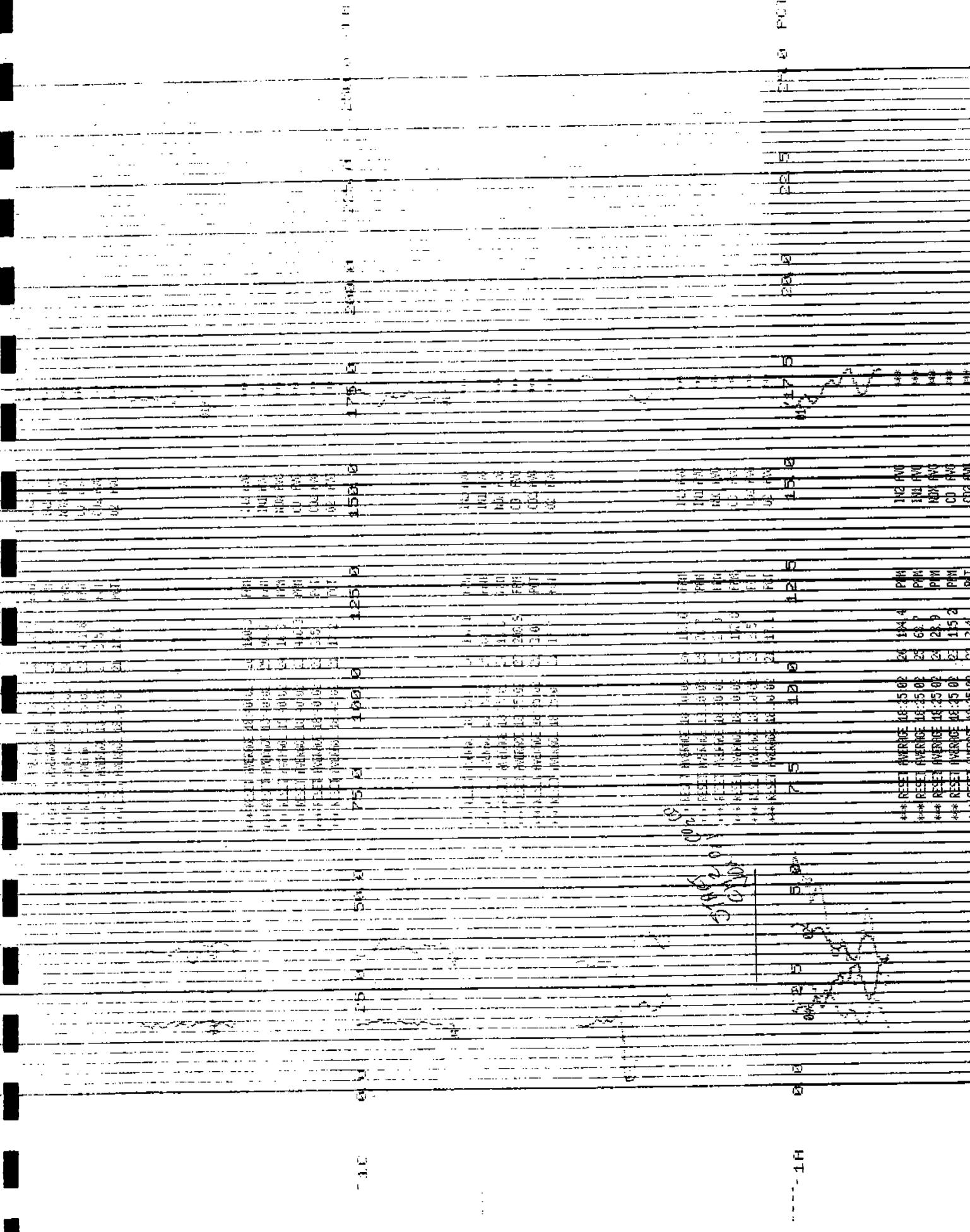
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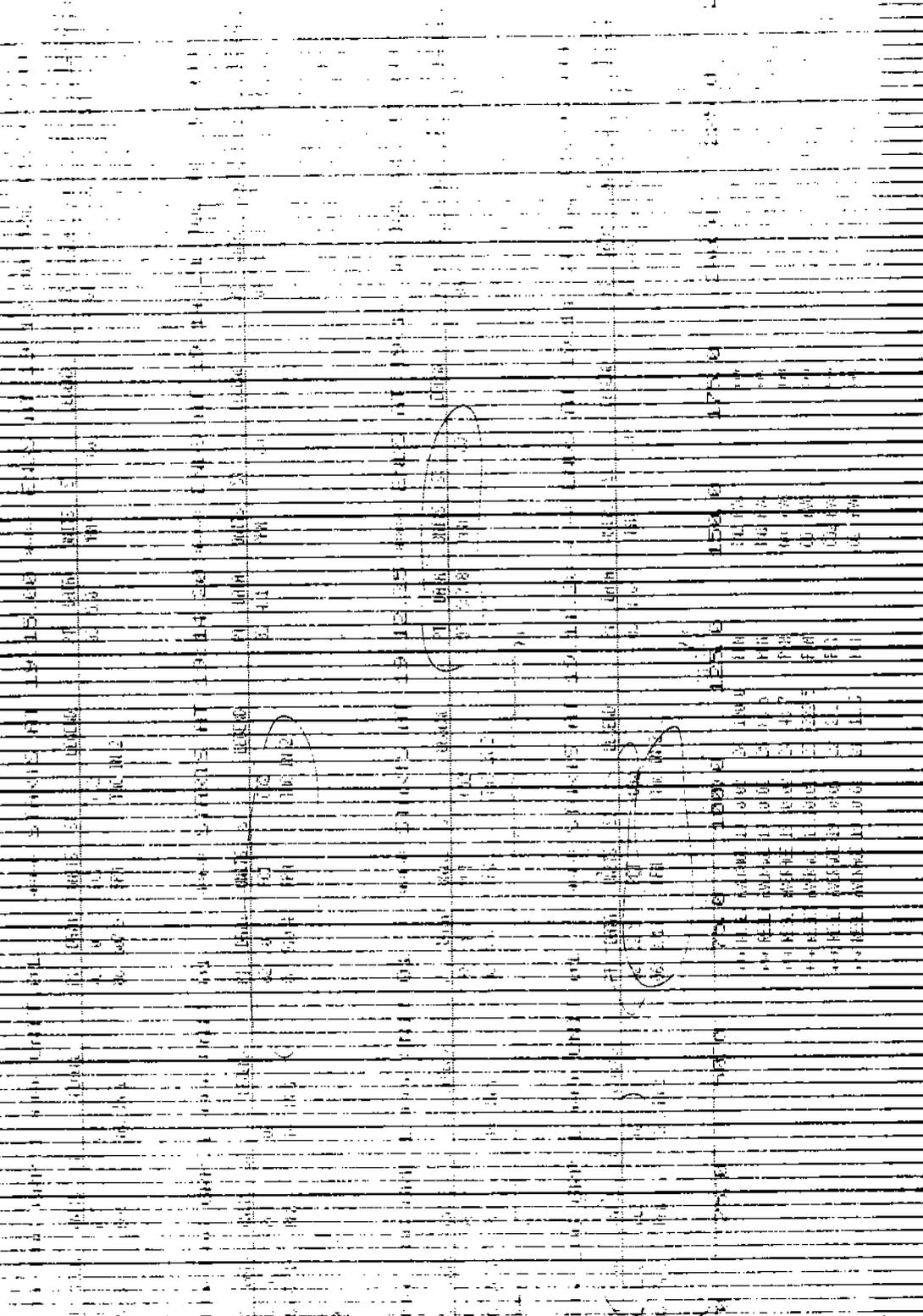


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SECTION

UNCO  
COA



PT	UNITS	ST	LEGEN	PT	UNITS	ST	LEGEN
42-1	PC	02		43	4.1	PPH	
06	P.A.		TIC IN 2				

PT	UNITS	ST	LEGEN	PT	UNITS	ST	LEGEN
42-1	PC	02		43	4.1	PPH	
06	P.A.		TIC IN 2				

PT	UNITS	ST	LEGEN	PT	UNITS	ST	LEGEN
42-1	PC	02		43	4.1	PPH	
06	P.A.		TIC IN 2				

PT	UNITS	ST	LEGEN	PT	UNITS	ST	LEGEN
42-1	PC	02		43	4.1	PPH	
06	P.A.		TIC IN 2				

STARTS AT 19:39:41

ENDS AT 19:39:42

JUL 09 09:52

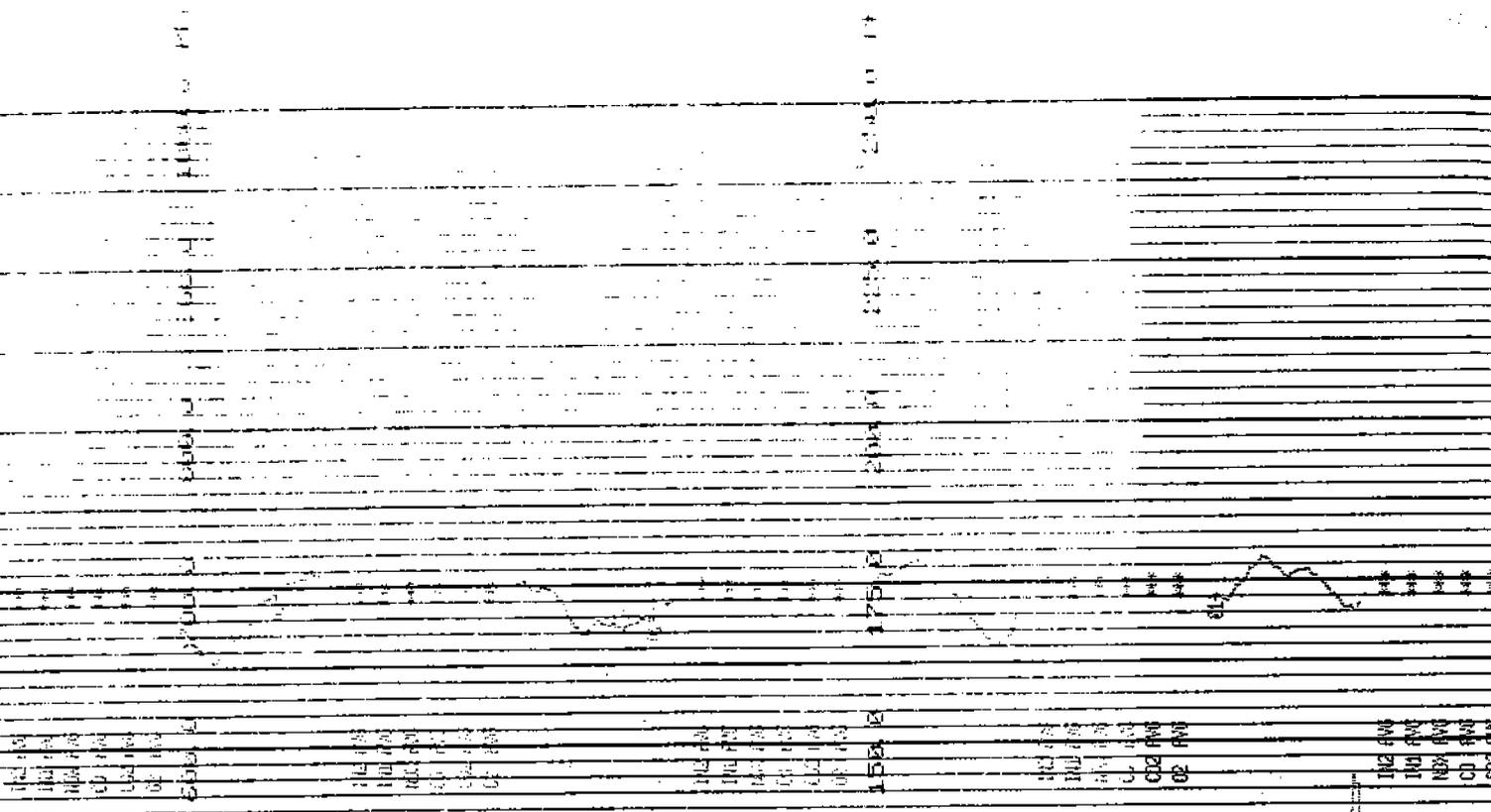
UNITS ST



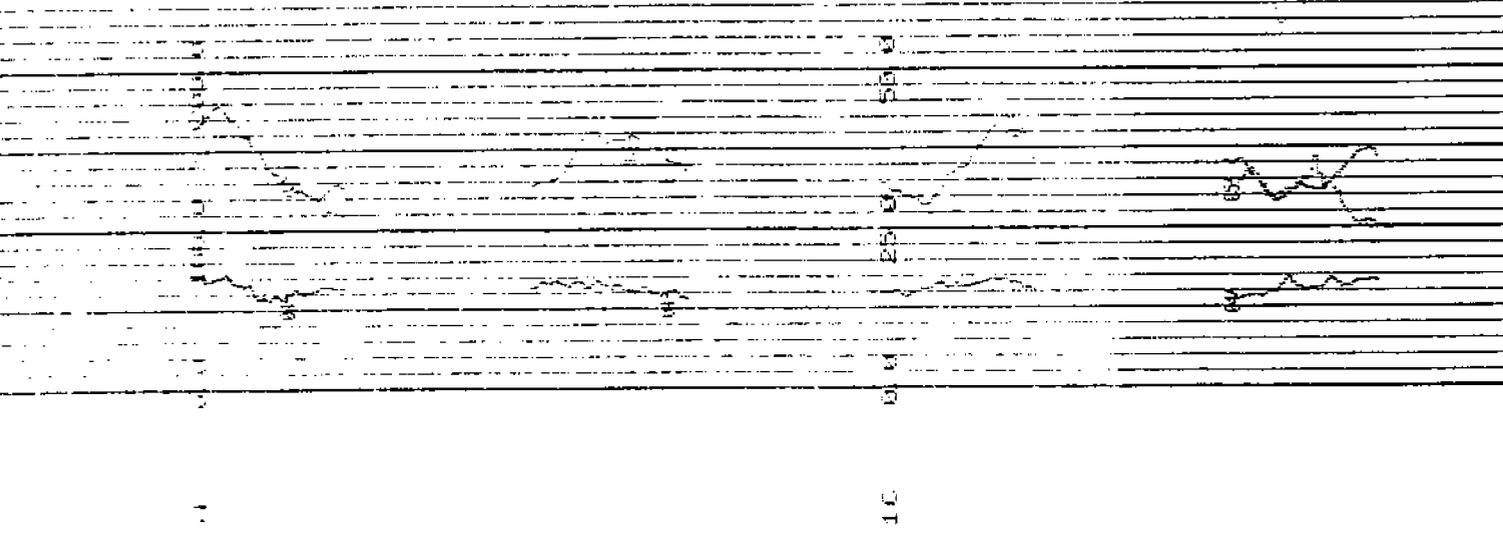








Parameter	50	75	100	125	150	175	200
INL AVG	50	75	100	125	150	175	200
INU AVG	50	75	100	125	150	175	200
INY AVG	50	75	100	125	150	175	200
CD AVG	50	75	100	125	150	175	200
CD2 AVG	50	75	100	125	150	175	200



Parameter	20	25	30	35	40	45	50
INL AVG	20	25	30	35	40	45	50
INU AVG	20	25	30	35	40	45	50
INY AVG	20	25	30	35	40	45	50
CD AVG	20	25	30	35	40	45	50
CD2 AVG	20	25	30	35	40	45	50











00458

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UNIT

UNIT	STARTS AT	ENDS AT	DATE
UNIT 33000	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 02	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 03	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 04	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 05	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 06	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 07	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 08	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 09	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 10	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 11	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 12	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 13	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 14	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 15	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 16	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 17	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 18	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 19	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 20	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 21	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 22	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 23	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 24	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 25	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 26	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 27	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 28	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 29	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 30	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 31	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 32	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 33	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 34	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 35	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 36	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 37	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 38	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 39	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 40	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 41	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 42	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 43	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 44	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 45	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 46	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 47	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 48	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 49	08:39:42	08:39:43	JUL 09, 1966
PT UNIT 50	08:39:42	08:39:43	JUL 09, 1966

CHART 1  
SITES Nos  
344



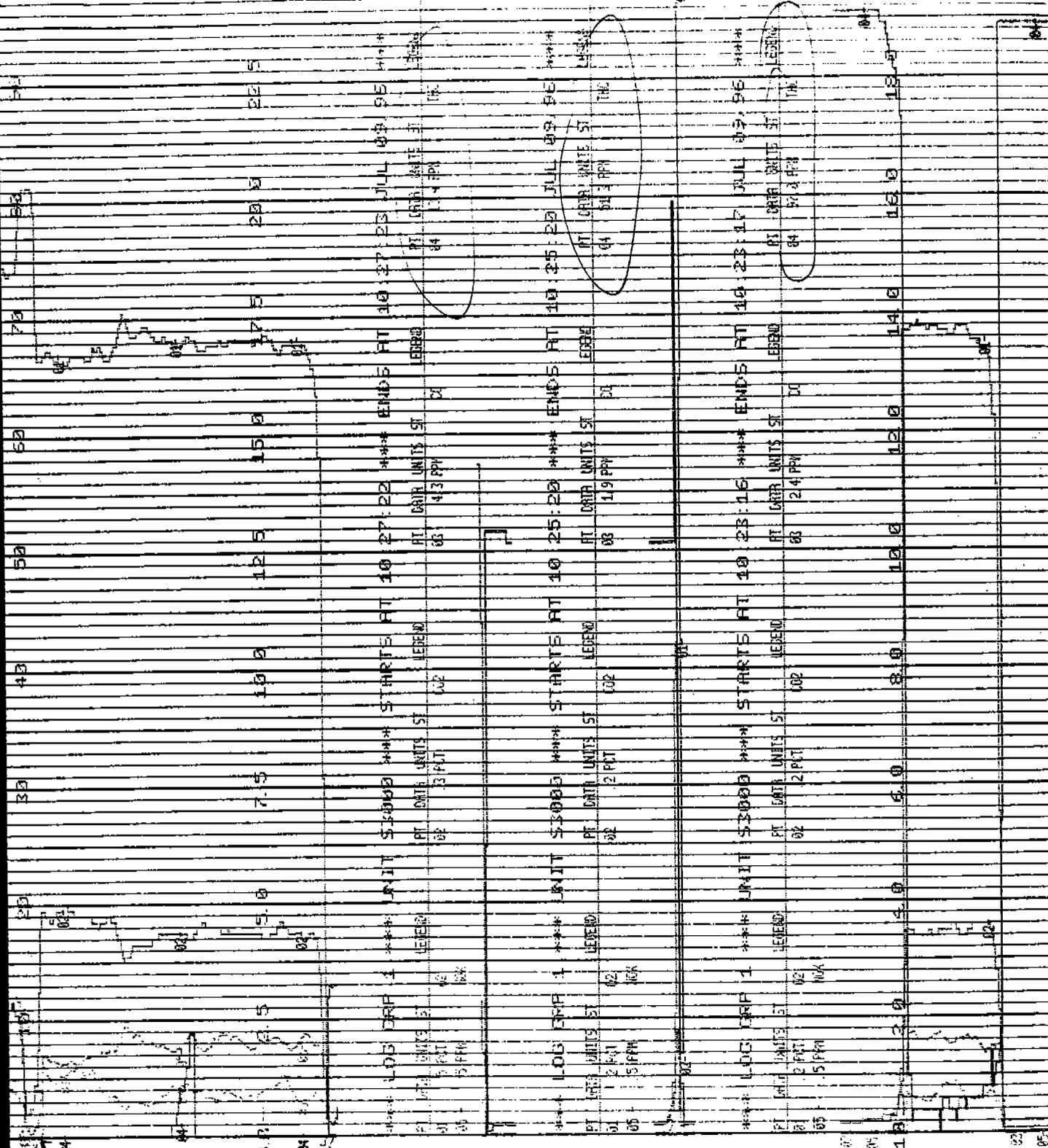




100 PPM

25.0 PCT

25.0 PCT



#3 In stack only

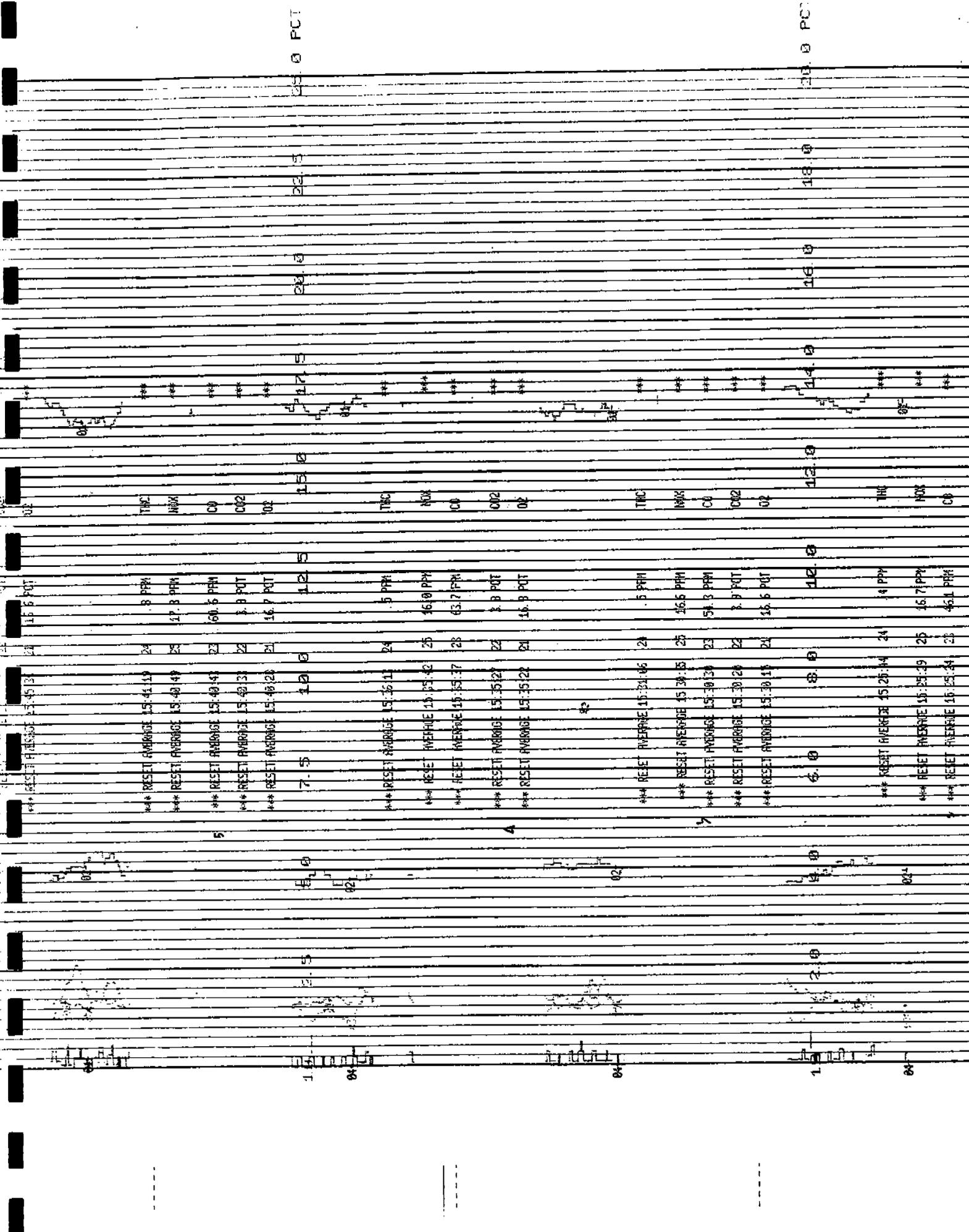
APL Stock

TH2

TH2

TH2





15.5 PCT

5

*** RESET AVERAGE	15:44:19	24	15.5 PCT
TMC	15:44:19	24	8 PPM
IMX	15:40:49	25	17.8 PPM
CO	15:40:49	23	50.5 PPM
CO2	15:40:13	22	3.8 PPT
O2	15:40:20	21	16.7 PPT

4

*** RESET AVERAGE	15:26:11	24	12.5
TMC	15:26:11	24	5 PPM
NOX	15:15:42	25	16.0 PPM
CO	15:15:37	28	63.7 PPM
CO2	15:35:27	23	3.8 PPT
O2	15:35:22	21	16.8 PPT

3

*** RESET AVERAGE	15:20:06	24	10.0
TMC	15:20:06	24	5 PPM
IMX	15:30:35	25	16.6 PPM
CO	15:30:30	23	51.3 PPM
CO2	15:30:20	22	3.9 PPT
O2	15:30:11	21	16.6 PPT

2

*** RESET AVERAGE	15:25:14	24	10.0
TMC	15:25:14	24	4 PPM
NOX	15:25:19	25	16.7 PPM
CO	15:25:14	23	46.1 PPM
CO2	15:25:11	21	4.0 PPT

15.5 PCT

12.5

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10.0 PCT

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253.0 PPM

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SMITH TO ELLIOTT

OKS

THO

NOX

CO

CO2

O2

THC

NOX

CO

CO2

O2

THO

NOX

CO

CO2

O2

THC

NOX

CO

CO2

O2

313 PPM

7.0 PPM

60.0 PPM

2.1 PPT

11.7 PPT

3.4 PPM

8.6 PPM

170.5 PPM

2.7 PPT

10.1 PPT

4.1 PPM

9.5 PPM

180.5 PPM

1.9 PPT

17.8 PPT

9 PPM

15.8 PPM

72.0 PPM

4.8 PPT

15.5 PPT

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RESET AVERAGE 16:01:17

RESET AVERAGE 16:20:14

RESET AVERAGE 16:01:11

RESET AVERAGE 16:01:00

RESET AVERAGE 16:00:53

RESET AVERAGE 15:55:44

RESET AVERAGE 15:55:20

RESET AVERAGE 15:55:04

RESET AVERAGE 15:55:14

RESET AVERAGE 15:55:14

RESET AVERAGE 15:50:34

RESET AVERAGE 15:41:01

RESET AVERAGE 15:50:56

RESET AVERAGE 15:50:44

RESET AVERAGE 15:50:43

RESET AVERAGE 15:46:27

RESET AVERAGE 15:45:57

RESET AVERAGE 15:45:51

RESET AVERAGE 15:45:41

RESET AVERAGE 15:45:34

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180.5 PPM

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RESET AVERAGE 16:01:17

RESET AVERAGE 16:20:14

RESET AVERAGE 16:01:11

RESET AVERAGE 16:01:00

RESET AVERAGE 16:00:53

RESET AVERAGE 15:55:44

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RESET AVERAGE 16:01:17

RESET AVERAGE 16:20:14

RESET AVERAGE 16:01:11

RESET AVERAGE 16:01:00

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RESET AVERAGE 16:01:17

RESET AVERAGE 16:20:14

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RESET AVERAGE 15:46:27

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RESET AVERAGE 15:45:51

RESET AVERAGE 15:45:41

RESET AVERAGE 15:45:34

313 PPM

7.0 PPM

60.0 PPM

2.1 PPT

11.7 PPT

3.4 PPM

8.6 PPM

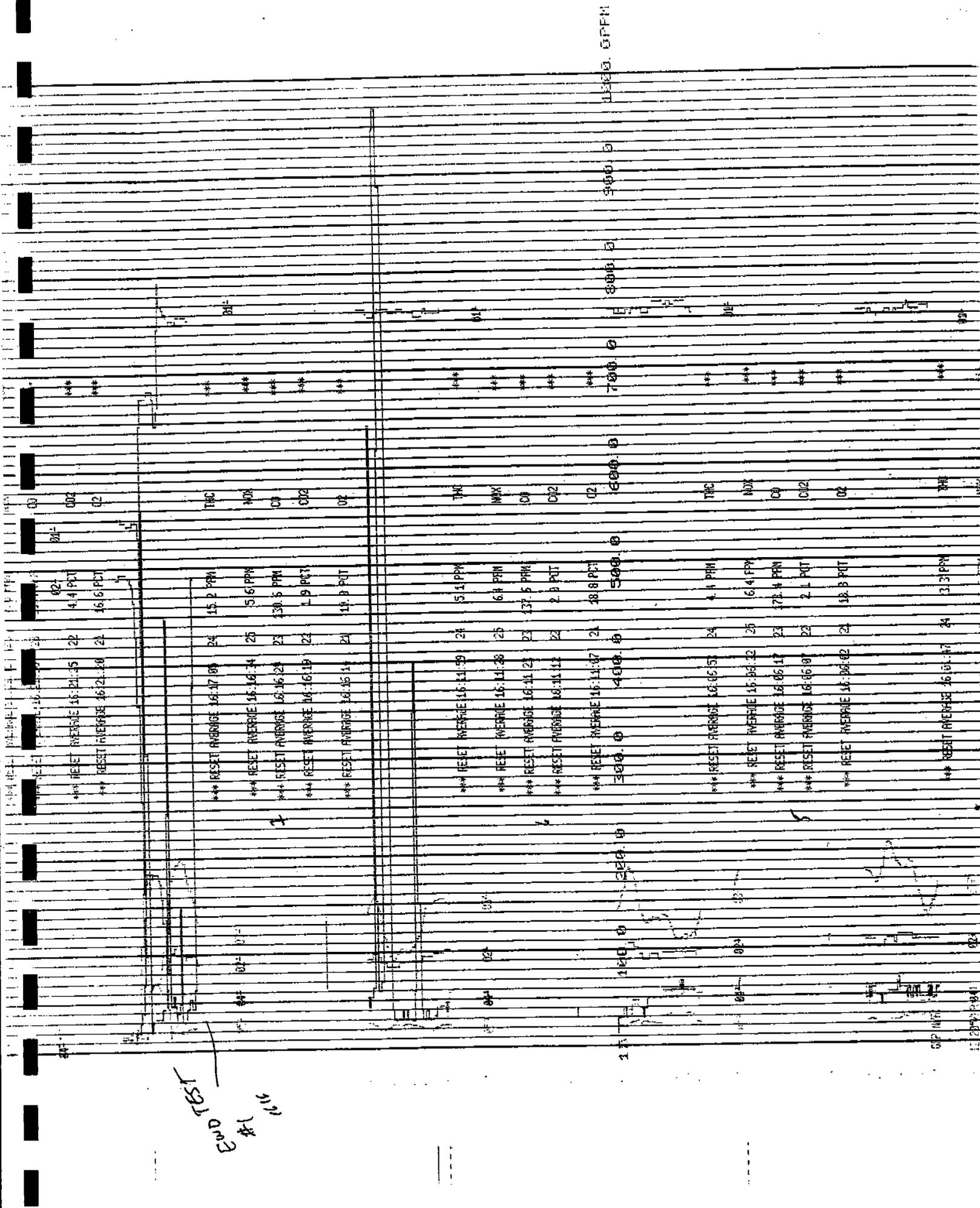
170.5 PPM

2.7 PPT

10.1 PPT

4.1 PPM

END TEST  
#1 11/2



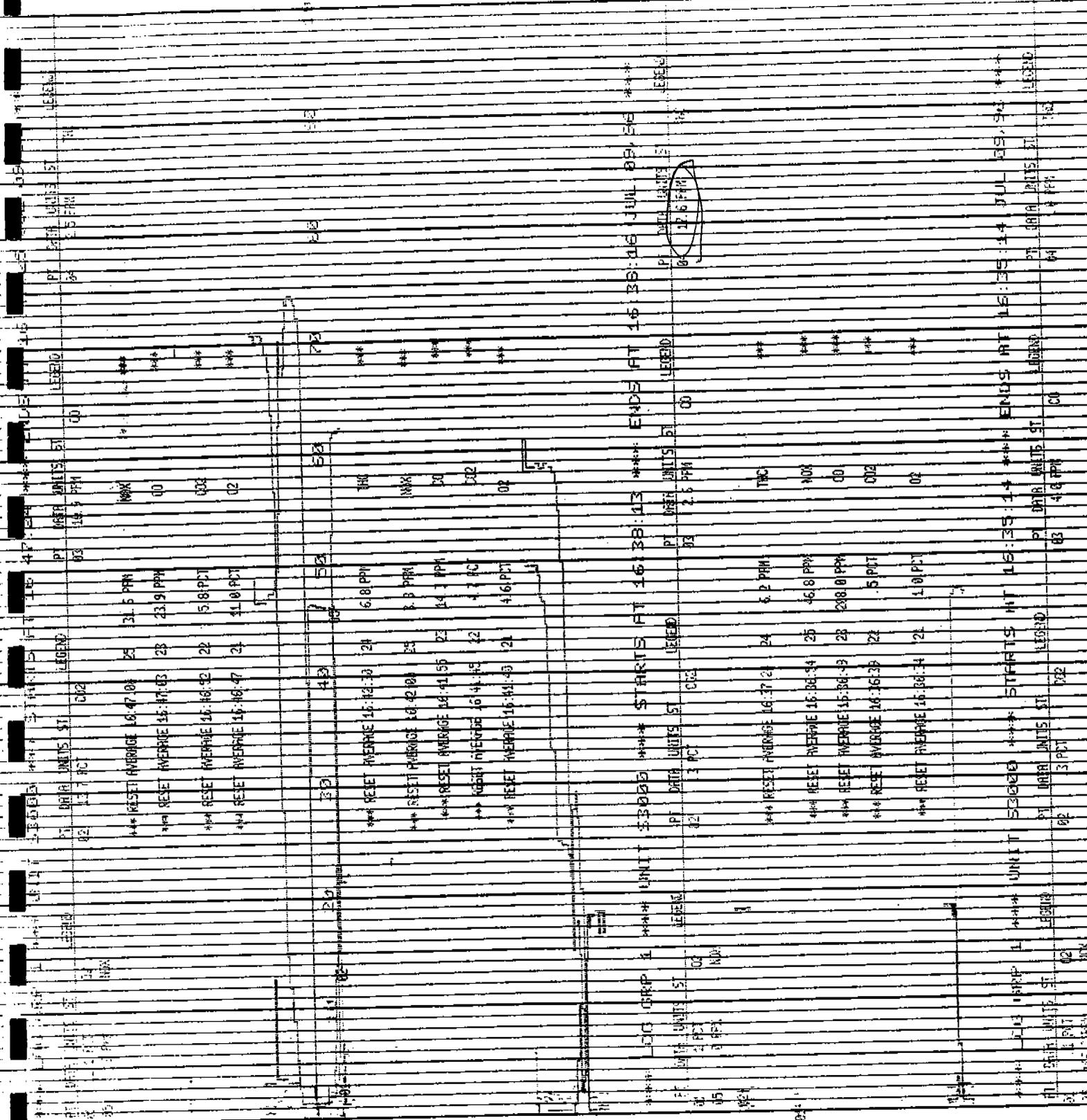


10/20

#3545825

774

102



LOG ORRP 1 UNIT 3000 \*\*\*\*\* STARTS AT 16:38:43 \*\*\*\*\* ENDS AT 16:38:16 JUL 09, 2008 \*\*\*\*\*

PT DATA UNITS ST LEGEND PT DATA UNITS ST LEGEND PT DATA UNITS ST LEGEND

02 1.1 PC 002 02 2.5 PPM 00 05 1.0 PPT 002 05 1.0 PPT 002 05 1.0 PPT 002

\*\*\*\*\* RESET AVERAGE 16:37:21 24 6.2 PPM TMC \*\*\*\*\*

\*\*\*\*\* RESET AVERAGE 16:36:14 25 46.8 PPM 10X \*\*\*\*\*

\*\*\*\*\* RESET AVERAGE 16:36:43 28 208.0 PPM 00 \*\*\*\*\*

\*\*\*\*\* RESET AVERAGE 16:36:33 22 5 PPT 002 \*\*\*\*\*

\*\*\*\*\* RESET AVERAGE 16:36:14 21 1.0 PPT 00 \*\*\*\*\*

UNIT 3000 \*\*\*\*\* STARTS AT 16:35:14 \*\*\*\*\* ENDS AT 16:35:14 JUL 09, 2008 \*\*\*\*\*

PT DATA UNITS ST LEGEND PT DATA UNITS ST LEGEND PT DATA UNITS ST LEGEND

02 1.1 PC 002 02 2.5 PPM 00 05 1.0 PPT 002 05 1.0 PPT 002 05 1.0 PPT 002

\*\*\*\*\* RESET AVERAGE 16:35:14 24 6.2 PPM TMC \*\*\*\*\*

\*\*\*\*\* RESET AVERAGE 16:35:14 25 46.8 PPM 10X \*\*\*\*\*

\*\*\*\*\* RESET AVERAGE 16:35:14 28 208.0 PPM 00 \*\*\*\*\*

\*\*\*\*\* RESET AVERAGE 16:35:14 22 5 PPT 002 \*\*\*\*\*

\*\*\*\*\* RESET AVERAGE 16:35:14 21 1.0 PPT 00 \*\*\*\*\*

250.0 PPM

225.0

200.0

175.0

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LOG GRP 1 UNIT S3000 STARTS AT 16:53:34 \*\*\* ENDS AT 16:53:34 JUL 09 '98 \*\*\*

PT DATA UNITS ST LEGRD 02 3 PPT 02 11.1 PPM 03 11.1 PPM 04 11.1 PPM 05 11.1 PPM 06 11.1 PPM 07 11.1 PPM 08 11.1 PPM 09 11.1 PPM 10 11.1 PPM 11 11.1 PPM 12 11.1 PPM 13 11.1 PPM 14 11.1 PPM 15 11.1 PPM 16 11.1 PPM 17 11.1 PPM 18 11.1 PPM 19 11.1 PPM 20 11.1 PPM 21 11.1 PPM 22 11.1 PPM 23 11.1 PPM 24 11.1 PPM 25 11.1 PPM 26 11.1 PPM 27 11.1 PPM 28 11.1 PPM 29 11.1 PPM 30 11.1 PPM 31 11.1 PPM 32 11.1 PPM 33 11.1 PPM 34 11.1 PPM 35 11.1 PPM 36 11.1 PPM 37 11.1 PPM 38 11.1 PPM 39 11.1 PPM 40 11.1 PPM 41 11.1 PPM 42 11.1 PPM 43 11.1 PPM 44 11.1 PPM 45 11.1 PPM 46 11.1 PPM 47 11.1 PPM 48 11.1 PPM 49 11.1 PPM 50 11.1 PPM 51 11.1 PPM 52 11.1 PPM 53 11.1 PPM 54 11.1 PPM 55 11.1 PPM 56 11.1 PPM 57 11.1 PPM 58 11.1 PPM 59 11.1 PPM 60 11.1 PPM 61 11.1 PPM 62 11.1 PPM 63 11.1 PPM 64 11.1 PPM 65 11.1 PPM 66 11.1 PPM 67 11.1 PPM 68 11.1 PPM 69 11.1 PPM 70 11.1 PPM 71 11.1 PPM 72 11.1 PPM 73 11.1 PPM 74 11.1 PPM 75 11.1 PPM 76 11.1 PPM 77 11.1 PPM 78 11.1 PPM 79 11.1 PPM 80 11.1 PPM 81 11.1 PPM 82 11.1 PPM 83 11.1 PPM 84 11.1 PPM 85 11.1 PPM 86 11.1 PPM 87 11.1 PPM 88 11.1 PPM 89 11.1 PPM 90 11.1 PPM 91 11.1 PPM 92 11.1 PPM 93 11.1 PPM 94 11.1 PPM 95 11.1 PPM 96 11.1 PPM 97 11.1 PPM 98 11.1 PPM 99 11.1 PPM 100 11.1 PPM

\*\*\* RESET AVERAGE 16:52:44 24 3.6 PPM \*\*\*

\*\*\* RESET AVERAGE 16:52:43 25 9 PPM \*\*\*

\*\*\* RESET AVERAGE 16:52:08 23 168.4 PPM \*\*\*

\*\*\* RESET AVERAGE 16:51:58 22 4.1 PCT \*\*\*

\*\*\* RESET AVERAGE 16:51:52 21 3.7 PCT \*\*\*

LOG GRP 1 UNIT S3200 STARTS AT 15:49:23 \*\*\* ENDS AT 15:49:23 JUL 09 '98 \*\*\*

PT DATA UNITS ST LEGRD 02 3 PPT 02 11.1 PPM 03 11.1 PPM 04 11.1 PPM 05 11.1 PPM 06 11.1 PPM 07 11.1 PPM 08 11.1 PPM 09 11.1 PPM 10 11.1 PPM 11 11.1 PPM 12 11.1 PPM 13 11.1 PPM 14 11.1 PPM 15 11.1 PPM 16 11.1 PPM 17 11.1 PPM 18 11.1 PPM 19 11.1 PPM 20 11.1 PPM 21 11.1 PPM 22 11.1 PPM 23 11.1 PPM 24 11.1 PPM 25 11.1 PPM 26 11.1 PPM 27 11.1 PPM 28 11.1 PPM 29 11.1 PPM 30 11.1 PPM 31 11.1 PPM 32 11.1 PPM 33 11.1 PPM 34 11.1 PPM 35 11.1 PPM 36 11.1 PPM 37 11.1 PPM 38 11.1 PPM 39 11.1 PPM 40 11.1 PPM 41 11.1 PPM 42 11.1 PPM 43 11.1 PPM 44 11.1 PPM 45 11.1 PPM 46 11.1 PPM 47 11.1 PPM 48 11.1 PPM 49 11.1 PPM 50 11.1 PPM 51 11.1 PPM 52 11.1 PPM 53 11.1 PPM 54 11.1 PPM 55 11.1 PPM 56 11.1 PPM 57 11.1 PPM 58 11.1 PPM 59 11.1 PPM 60 11.1 PPM 61 11.1 PPM 62 11.1 PPM 63 11.1 PPM 64 11.1 PPM 65 11.1 PPM 66 11.1 PPM 67 11.1 PPM 68 11.1 PPM 69 11.1 PPM 70 11.1 PPM 71 11.1 PPM 72 11.1 PPM 73 11.1 PPM 74 11.1 PPM 75 11.1 PPM 76 11.1 PPM 77 11.1 PPM 78 11.1 PPM 79 11.1 PPM 80 11.1 PPM 81 11.1 PPM 82 11.1 PPM 83 11.1 PPM 84 11.1 PPM 85 11.1 PPM 86 11.1 PPM 87 11.1 PPM 88 11.1 PPM 89 11.1 PPM 90 11.1 PPM 91 11.1 PPM 92 11.1 PPM 93 11.1 PPM 94 11.1 PPM 95 11.1 PPM 96 11.1 PPM 97 11.1 PPM 98 11.1 PPM 99 11.1 PPM 100 11.1 PPM

\*\*\* RESET AVERAGE 15:47:38 24 1.6 PPM \*\*\*

LOG GRP 1 UNIT S3000 STARTS AT 16:47:24 \*\*\* ENDS AT 16:47:25 JUL 09 '98 \*\*\*

PT DATA UNITS ST LEGRD 02 3 PPT 02 11.1 PPM 03 11.1 PPM 04 11.1 PPM 05 11.1 PPM 06 11.1 PPM 07 11.1 PPM 08 11.1 PPM 09 11.1 PPM 10 11.1 PPM 11 11.1 PPM 12 11.1 PPM 13 11.1 PPM 14 11.1 PPM 15 11.1 PPM 16 11.1 PPM 17 11.1 PPM 18 11.1 PPM 19 11.1 PPM 20 11.1 PPM 21 11.1 PPM 22 11.1 PPM 23 11.1 PPM 24 11.1 PPM 25 11.1 PPM 26 11.1 PPM 27 11.1 PPM 28 11.1 PPM 29 11.1 PPM 30 11.1 PPM 31 11.1 PPM 32 11.1 PPM 33 11.1 PPM 34 11.1 PPM 35 11.1 PPM 36 11.1 PPM 37 11.1 PPM 38 11.1 PPM 39 11.1 PPM 40 11.1 PPM 41 11.1 PPM 42 11.1 PPM 43 11.1 PPM 44 11.1 PPM 45 11.1 PPM 46 11.1 PPM 47 11.1 PPM 48 11.1 PPM 49 11.1 PPM 50 11.1 PPM 51 11.1 PPM 52 11.1 PPM 53 11.1 PPM 54 11.1 PPM 55 11.1 PPM 56 11.1 PPM 57 11.1 PPM 58 11.1 PPM 59 11.1 PPM 60 11.1 PPM 61 11.1 PPM 62 11.1 PPM 63 11.1 PPM 64 11.1 PPM 65 11.1 PPM 66 11.1 PPM 67 11.1 PPM 68 11.1 PPM 69 11.1 PPM 70 11.1 PPM 71 11.1 PPM 72 11.1 PPM 73 11.1 PPM 74 11.1 PPM 75 11.1 PPM 76 11.1 PPM 77 11.1 PPM 78 11.1 PPM 79 11.1 PPM 80 11.1 PPM 81 11.1 PPM 82 11.1 PPM 83 11.1 PPM 84 11.1 PPM 85 11.1 PPM 86 11.1 PPM 87 11.1 PPM 88 11.1 PPM 89 11.1 PPM 90 11.1 PPM 91 11.1 PPM 92 11.1 PPM 93 11.1 PPM 94 11.1 PPM 95 11.1 PPM 96 11.1 PPM 97 11.1 PPM 98 11.1 PPM 99 11.1 PPM 100 11.1 PPM

\*\*\* RESET AVERAGE 16:47:24 24 1.6 PPM \*\*\*

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NOC

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2411.9 PPM

\*\*\* RESET AVERAGE 18:16:24 25 48.6 PPM

\*\*\* RESET AVERAGE 18:25:24 24 16.2 PPM

\*\*\* RESET AVERAGE 18:26:19 22 5.5 PPM

\*\*\* RESET AVERAGE 18:26:01 11 16.7 PPM

\*\*\* RESET AVERAGE 18:22:45 28 339.3 PPM

\*\*\* RESET AVERAGE 18:24:38 25 188 PPM

\*\*\* RESET AVERAGE 18:24:48 24 16.9 PPM

\*\*\* RESET AVERAGE 18:24:18 24 16.9 PPM

\*\*\* RESET AVERAGE 18:21:13 22 5.4 PPM

\*\*\* RESET AVERAGE 18:20:54 24 16.5 PPM

\*\*\* RESET AVERAGE 18:16:14 25 18.5 PPM

\*\*\* RESET AVERAGE 18:16:33 24 7.4 PPM

\*\*\* RESET AVERAGE 18:16:06 23 262.2 PPM

\*\*\* RESET AVERAGE 18:16:04 22 5.1 PPM

\*\*\* RESET AVERAGE 18:15:54 21 15.5 PPM

\*\*\* PRINTER ON 18:13:15 JUL 69.96

\*\*\* PRINTER OFF 17:55:18 JUL 69.96

\*\*\* RESET AVERAGE 17:55:16 25 14.7 PPM

\*\*\* RESET AVERAGE 17:54:41 24 3.4 PPM

*Reset 1965*

20.5

22.5

20.5

17.5

15.0

12.5

10.0

7.5

5.0

2.5

0.0

20.5

20.5







250.0 PPH

225.0

200.0

175.0

150.0

125.0

100.0

75.0

50.0

25.0

0.0

UNIT 53000 \*\*\*\*\* STARTS AT 19:35:41 \*\*\*\*\* ENDS AT 19:35:42 JUL 09:56 \*\*\*\*\*

PT DATA UNITS ST LEGEND

02 7 PPT (02)

04 4.2 PPH

UNIT 53000 \*\*\*\*\* STARTS AT 19:33:45 \*\*\*\*\* ENDS AT 19:33:46 JUL 09:56 \*\*\*\*\*

PT DATA UNITS ST LEGEND

02 7 PPT (02)

04 4.4 PPH

UNIT 53000 \*\*\*\*\* STARTS AT 19:32:04 \*\*\*\*\* ENDS AT 19:32:08 JUL 09:56 \*\*\*\*\*

PT DATA UNITS ST LEGEND

02 12.5 PPT (02)

04 1.8 PPH

UNIT 53000 \*\*\*\*\* STARTS AT 19:31:02 \*\*\*\*\* ENDS AT 19:31:03 JUL 09:56 \*\*\*\*\*

PT DATA UNITS ST LEGEND

02 12.5 PPT (02)

04 1.8 PPH

UNIT 53000 \*\*\*\*\* STARTS AT 19:28:09 \*\*\*\*\* ENDS AT 19:28:09 JUL 09:56 \*\*\*\*\*

PT DATA UNITS ST LEGEND

02 12.1 PPT (02)

04 2.9 PPH

60

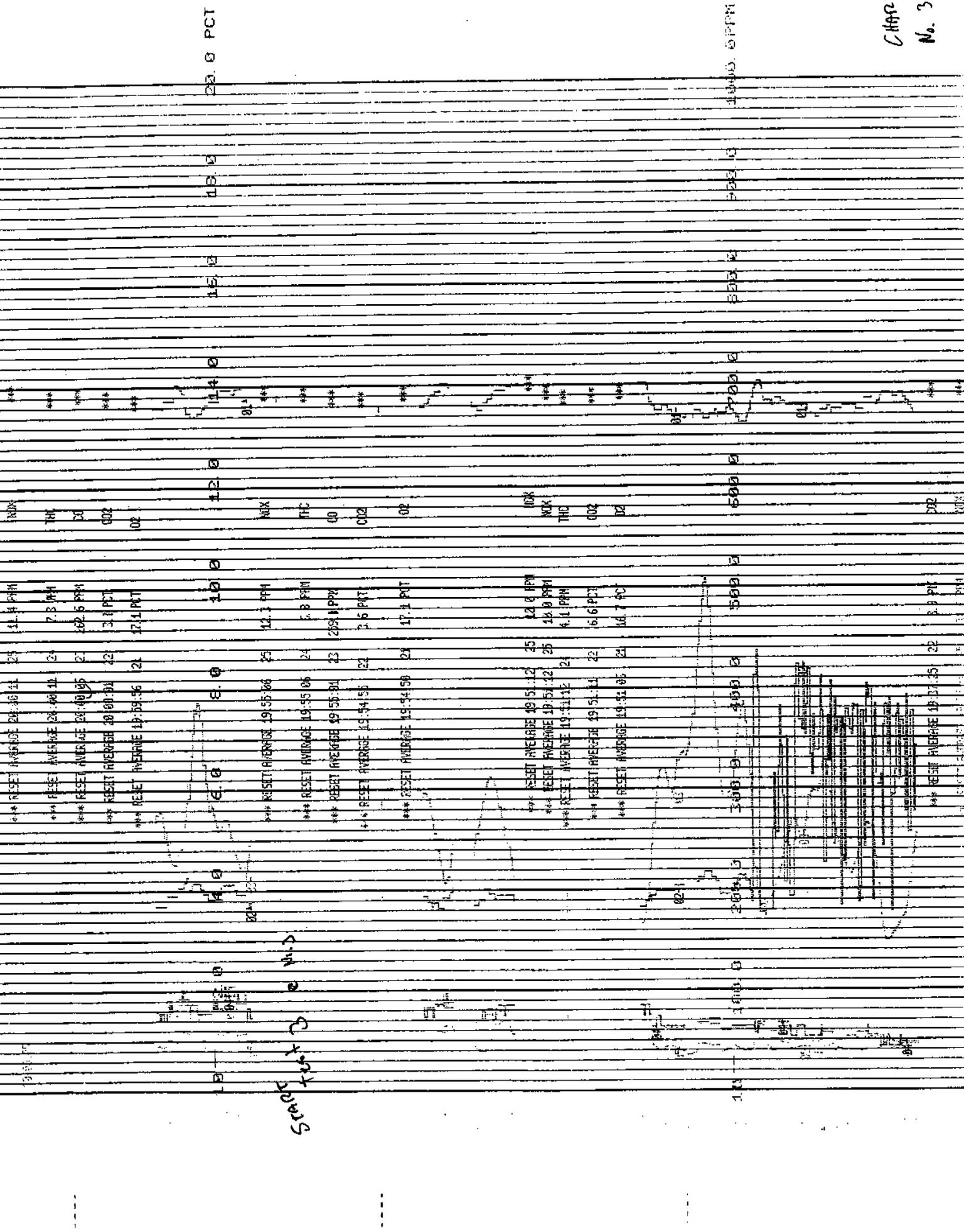
100

100

100

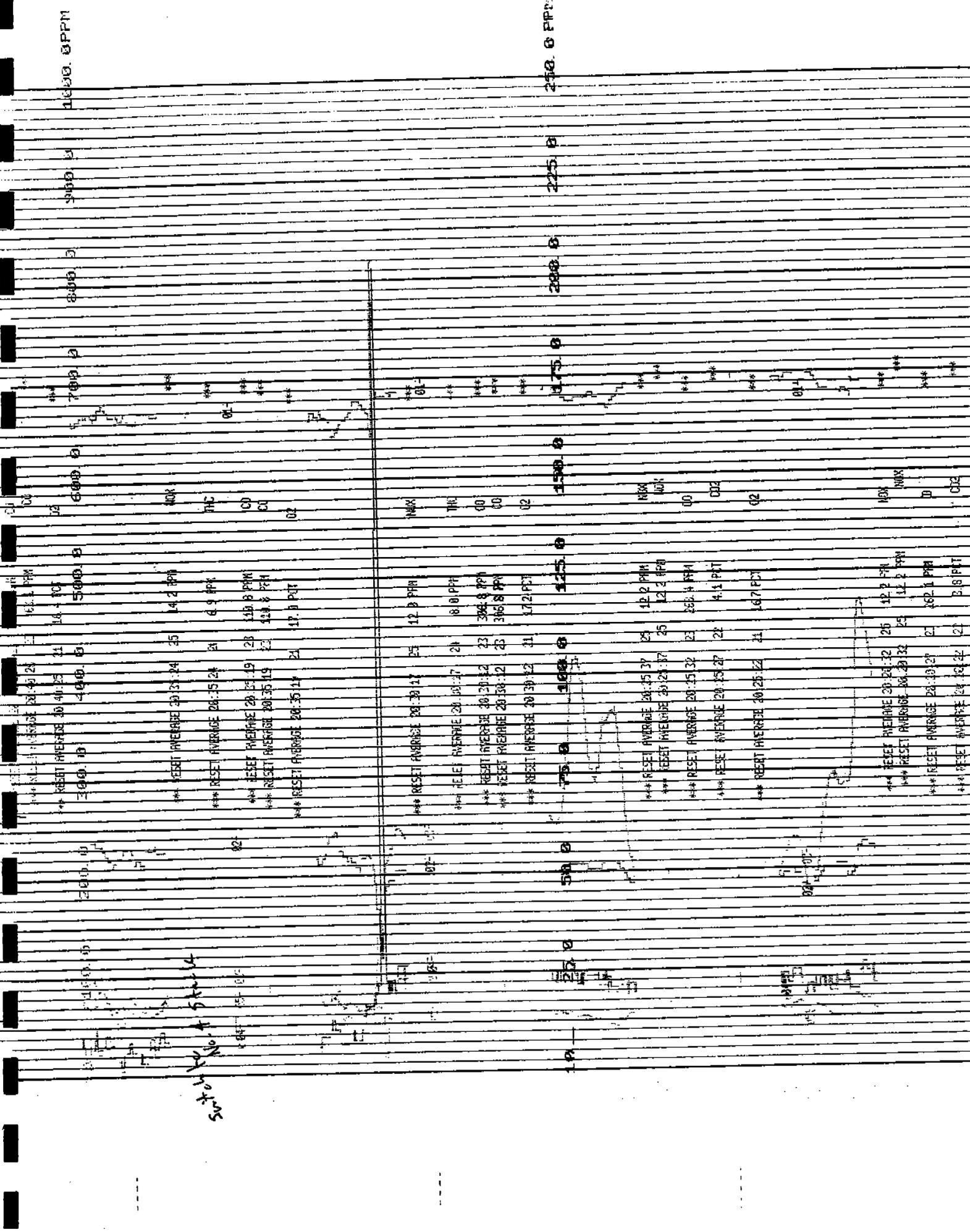
5-12 6:17 No. 3

SEARCH TANK 3 e No. 5





Sum to No. 4 Scale



1000.0 PPM

800.0

600.0

400.0

200.0

0

200.0

400.0

600.0

800.0

1000.0

1200.0

1400.0

1600.0

1800.0

2000.0

2200.0

2400.0 PPM

01

02

03

04

05

06

07

08

09

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14

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21

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18

19

20

21

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23

24

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31

32

→ END 7850 3

\*\*\* RESET AVERAGE 20:55:52 25 15.4 PPM

\*\*\* RESET AVERAGE 20:55:52 24 1.2 PPM

\*\*\* RESET AVERAGE 20:55:47 21 68.0 PPM

\*\*\* RESET AVERAGE 20:55:47 28 68.0 PPM

\*\*\* RESET AVERAGE 20:55:46 21 15.4 PPM

\*\*\* RESET AVERAGE 20:50:44 22 15.8 PPM

\*\*\* RESET AVERAGE 20:50:44 24 1.6 PPM

\*\*\* RESET AVERAGE 20:50:46 23 55.2 PPM

\*\*\* RESET AVERAGE 20:50:46 23 64.2 PPM

\*\*\* RESET AVERAGE 20:50:39 21 16.1 PPM

\*\*\* RESET AVERAGE 20:45:16 25 16.3 PPM

\*\*\* RESET AVERAGE 20:45:16 24 1.3 PPM

\*\*\* RESET AVERAGE 20:45:13 23 63.9 PPM

\*\*\* RESET AVERAGE 20:45:13 23 53.9 PPM

\*\*\* RESET AVERAGE 20:45:13 21 15.1 PPM

\*\*\* RESET AVERAGE 20:40:30 25 15.7 PPM

\*\*\* RESET AVERAGE 20:40:30 24 1.5 PPM

\*\*\* RESET AVERAGE 20:40:25 21 63.1 PPM

\*\*\* RESET AVERAGE 20:40:26 22 63.1 PPM

\*\*\* RESET AVERAGE 20:40:25 21 14.4 PPM

NDX

THU

01

02

NDX

THU

00

01

02

NDX

THU

01

02

NDX

THU

01

02

23.0 PCT

18.0

16.0

14.0

12.0

10.0

8.0

6.0

4.0

2.0

0.0

0.0

0.0

No. 3  
Sys Bins

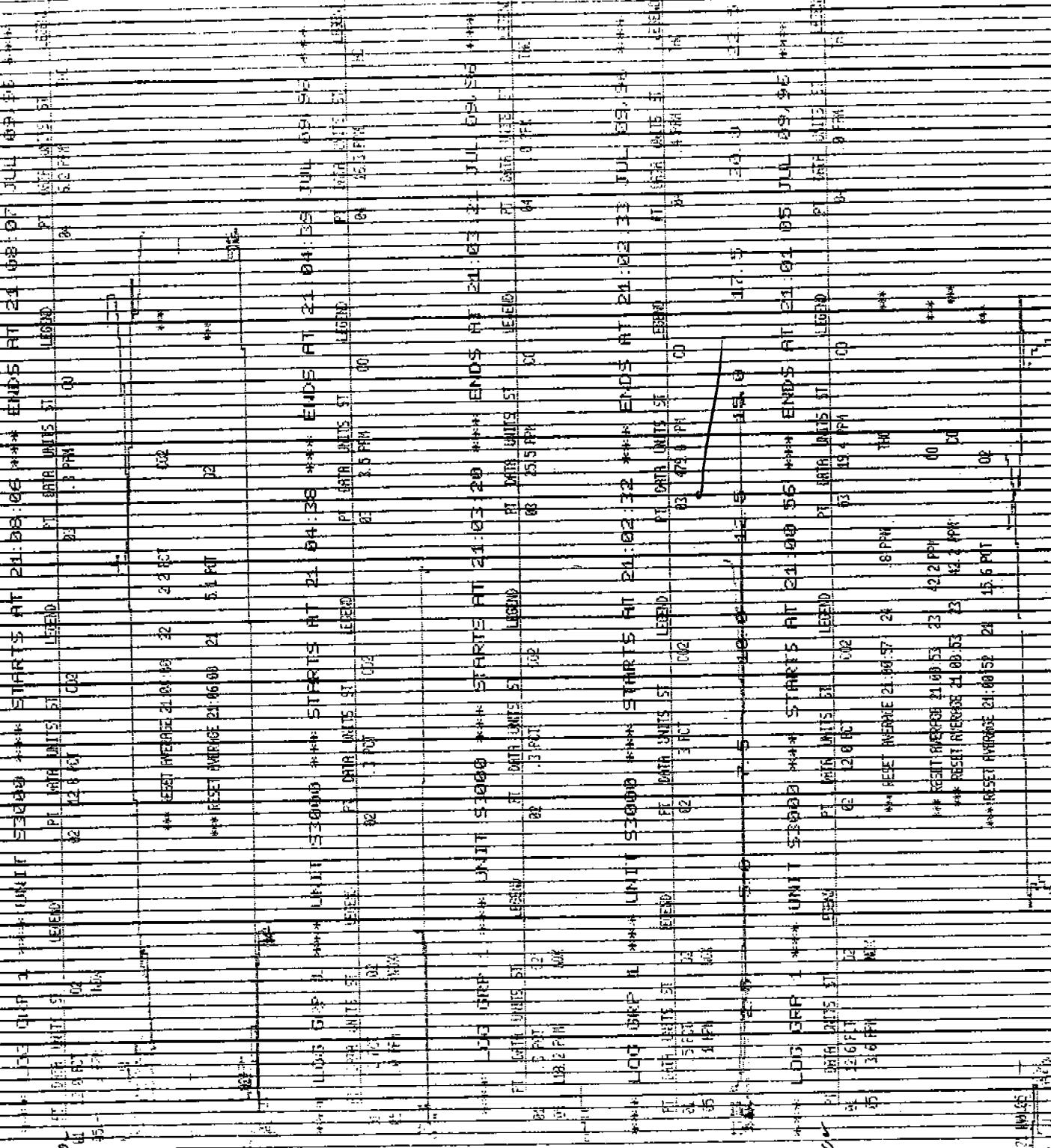
TAU

NO. 1

00

No. 4  
Sys Bins

25.0



\*\*\* SYSTEM RESTART 21:35:16 JUL 08, 96 \*\*\*  
 \*\*\* PRINTER OFF 21:16:32 JUL 08, 96 \*\*\*  
 \*\*\* RESET AVERAGE 21:16:25 45.8 PPM NOX  
 \*\*\* RESET AVERAGE 21:35:16 24 6.5 PPM THO  
 \*\*\* RESET AVERAGE 21:15:11 21 288.5 PPM CO  
 \*\*\* RESET AVERAGE 21:04:11 20 288.5 PPM CO  
 \*\*\* RESET AVERAGE 21:04:11 21 5.5 PPM O2

\*\*\* LOG OFF 1 \*\*\* UNIT 53000 \*\*\* STARTS AT 21:13:34 \*\*\* ENDS AT 21:13:36 JUL 08, 96 \*\*\*  
 PT DATA UNITS ST LEGND PT DATA UNITS ST LEGND  
 O2 2 PPT CO 08 37 PPM O2  
 CO 30 NO 1150 60 79 80 98

NOX

\*\*\* LOG OFF 1 \*\*\* UNIT 53000 \*\*\* STARTS AT 21:11:34 \*\*\* ENDS AT 21:11:36 JUL 08, 96 \*\*\*  
 PT DATA UNITS ST LEGND PT DATA UNITS ST LEGND  
 O2 3 PPT CO 03 46.8 PPM NOX  
 CO 30 NO 1150 60 79 80 98

CO

\*\*\* RESET AVERAGE 21:11:10 35 4.5 PPM NOX  
 \*\*\* RESET AVERAGE 21:11:10 24 5.5 PPM THO  
 \*\*\* RESET AVERAGE 21:11:06 28 86.8 PPM CO  
 \*\*\* RESET AVERAGE 21:11:04 23 86.8 PPM CO  
 \*\*\* RESET AVERAGE 21:11:05 21 4.4 PPM O2

\*\*\* LOG OFF 1 \*\*\* UNIT 53000 \*\*\* STARTS AT 21:08:06 \*\*\* ENDS AT 21:08:07 JUL 08, 96 \*\*\*  
 PT DATA UNITS ST LEGND PT DATA UNITS ST LEGND

**DRYER JULY 9th, 1996**

**NOX,CO,VOC,CO2,O2**

DATA TIME:	START=	15:10	END=	17:50	HOURS=	2.67
	START=	18:10	END=	21:00	HOURS=	2.83
					TOTAL=	<u>5.50</u>

**BOARD WEIGHTS - LBS**

average weights determined by taking every 25th untrimmed board (from press tapes)

7/16"		201.6 lb= average
per/peice	46.87	untrimmed
per/ 8' x 16'	187.48	mat weight
		7.0% =trim %

**PLANT PRODUCTION RATE**

5.50 =hours during testing  
95 =pressloads  
1,140 =no. of 8'x16' boards produced (pressloads x 12 boards per load)  
145,920 =volume produced in surface footage ( pressloads x 8'x16'x12 openings)  
170,245 =volume produced 3/8" basis ( pressloads x 8'x16'x 12 openings x 1.1667)  
213,732 =lbs of finished product (boards produced x weight of finished board)  
38,860 =lbs of finished product per hour (lbs of finshed product / hours)  
19.43 =tons of finished product per hour (lbs of finshed product per hour / 2000 lb)

**FUEL BURNING RATE ESTIMATED BY DRY FUEL INPUT**

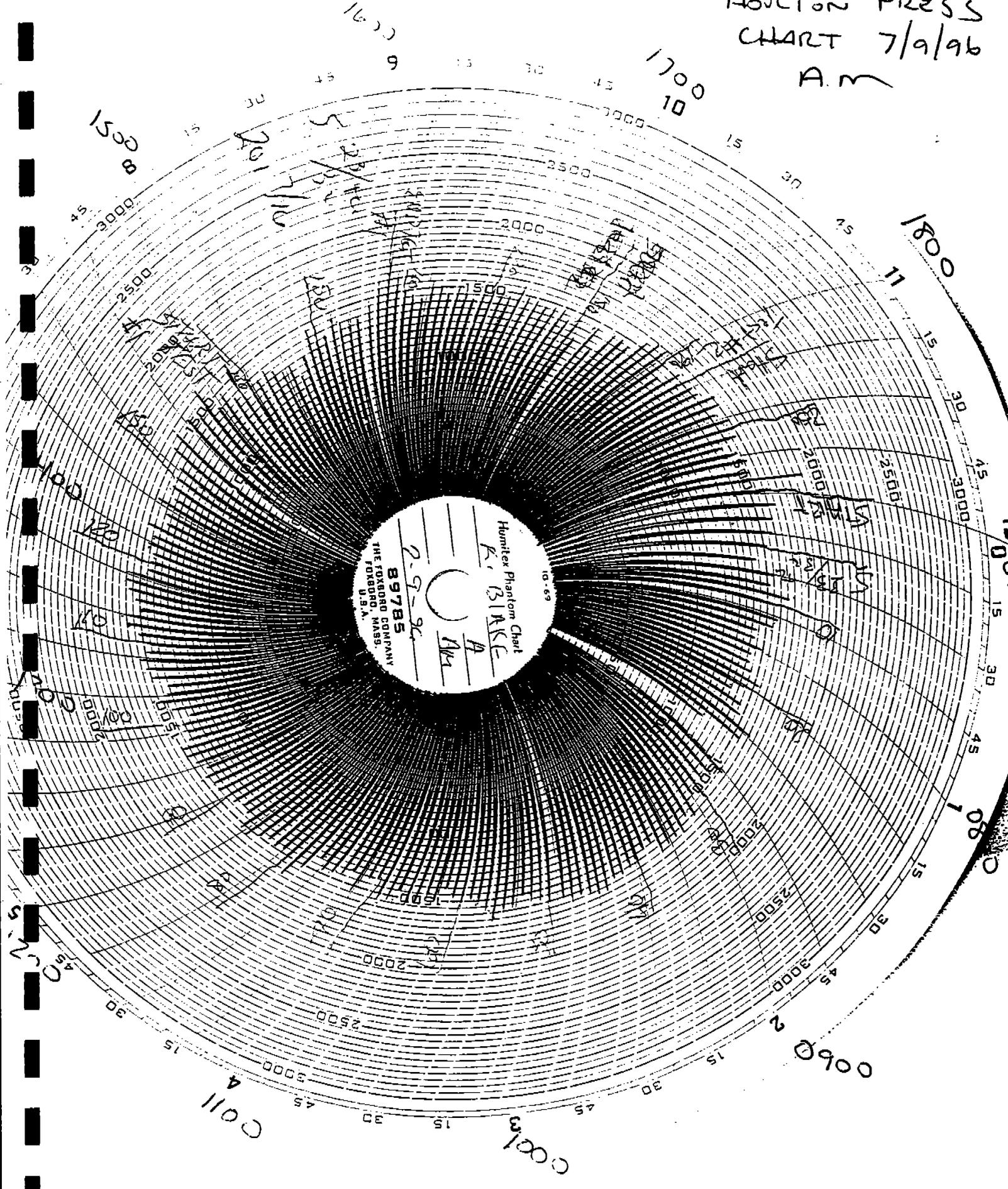
**SURFACE**

5.71 =SURFACE fuel calibration in pounds per count  
2,811 =SURFACE counts during testing hours  
16,051 =SURFACE lbs of fuel burned during testing  
5.50 =hours during testing  
2,918 =lbs of dry fuel burned per hour during testing (pounds of dry fuel / testing hours)  
1.46 =tons of dry fuel burned per hour during testing (pounds of dry fuel / 2000 lbs)  
8,500 =estimated BTU content per pound of dry fuel,  
24.8 =estimated mmbtu input per hour (lbs of dry fuel per hour x btu content)  
1,107 =average inlet temperature  
33.05 =average incoming moisture percent  
7.67 =average dry moisture percent

**CORE**

6.29 =CORE fuel calibration in pounds per count  
2,464 =CORE counts during testing hours  
15,499 =CORE lbs of fuel burned during testing  
5.50 =hours during testing  
2,818 =lbs of dry fuel burned per hour during testing (pounds of dry fuel / testing hours)  
1.41 =tons of dry fuel burned per hour during testing (pounds of dry fuel / 2000 lbs)  
8,500 =estimated BTU content per pound of dry fuel,  
24.0 =estimated mmbtu input per hour (lbs of dry fuel per hour x btu content)  
1,229 =average inlet temperature  
33.05 =average incoming moisture percent  
4.67 =average dry moisture percent

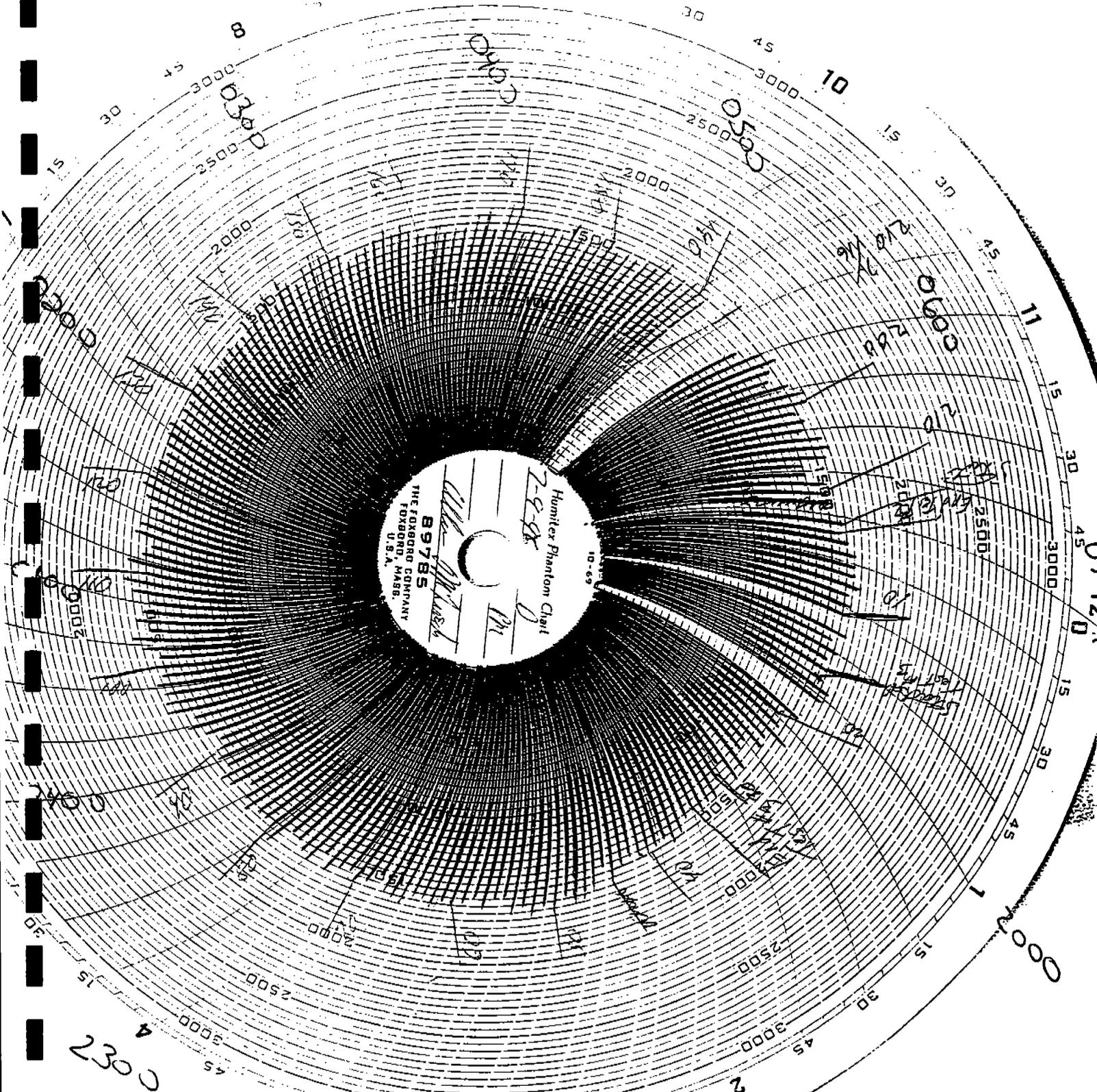
Houlton Press  
Chart 7/9/96  
A.M



Humitex Phantom Chart  
 K. B. KSC  
 A  
 M  
 2-9-96  
 89785  
 THE FOXBORO COMPANY  
 FOXBORO, MASS.  
 U.S.A.  
 10-69

7

HUTTON PRESS  
 CHART 7/9/96  
 P.M



2300

2200

2100 PRESSLOADS

15:10 - 17:50 = 47  
 18:10 - 21:00 = 48  
 95





LOUISIANA-PACIFIC  
DULTON, MAINE

# SHIFT OPERATING REPORT

911.C. <sup>CC</sup>

SUPERVISOR Prescott SHIFT \_\_\_\_\_ AM/PM PM CREW A DATE 7-9-96

**PRESS OPERATION:**

THICKNESS	PRESSLOADS	3/8" TIG	DOWNTIME (Mins)			
			M	E	O	QC
1/16	201	360202				
3/32 TIG	5	14720				
TOTAL	206	374922	3	8	4	

**YARD OPERATIONS:**

FIRE DUMP CLEANED	<u>3</u>	TIMES
TRUCKS USED DIRECT	_____	TRUCKS
BACK TRUCKS LOADED	_____	TRAILERS
MISCELLANEOUS	_____	

KONUS FURNACE	HRS. FUEL USAGE WOOD	HRS. FUEL USAGE OIL
#1	0	
#2	12 Hours	

**DRYER OPERATION:**

	DRY FUEL USAGE LBS.	OIL FUEL USAGE HRS.	AVE. INLET TEMP	RUNNING TIME MINS.	DOWN TIME	AVG. WET MOISTURE	AVG. DRY MOISTURE	REASON FOR OIL USAGE
CORE	7,810	0	1153	718	2	43.4%	4.6%	NONE USE
RFACE	8,420	41 minutes	1115	705	15	47.8%	7.6%	Water Short

# OF UNITS	1/4	5/16	3/8	7/16	15/32	1/2	19/32	23/32 TIG	OTHER
A				107				4+46 Pc	
1/2 UNITS				17 Pc					
U				1 Pc					
E & X									

LESS THAN 99.5%, WHY?

**\*\*\*MAINTENANCE/LOCK-OUT LOG\*\*\***

MOTOR #	LOCKED OUT	FROM	TO	BRIEF DESCRIPTION OF WORK BEING DONE	INITIALS OF PERSON LOCKING OUT

**PERSONNEL COMMENTS/CONCERNS:**

SENT/TARDY	REASON	EXTRA PERSONNEL	REASON

LOUISIANA-PACIFIC  
BOULTON, MAINE

# SHIFT OPERATING REPORT

91.0 (RE)  
S.C.  
49

SUPERVISOR T. Tower

SHIFT \_\_\_\_\_

AM  
PM

CREW D

DATE 7/9/96

**PRESS OPERATION:**

THICKNESS	PRESSLOADS	3/8" FTC	DOWNTIME (Mins)			
			M	E	O	QC
7/16						
TOTAL	210	376 33 1	19			8

**YARD OPERATIONS:**

FIRE DUMP CLEANED	<u>0</u>	TIMES
TRUCKS USED DIRECT	_____	TRUCKS
BARK TRUCKS LOADED	_____	TRAILERS
MISCELLANEOUS	_____	

KONUS FURNACE	HRS. FUEL USAGE WOOD	HRS. FUEL USAGE OIL
#1	0	0
#2	12 hrs.	0

**DRYER OPERATION:**

	DRY FUEL USAGE LBS.	OIL FUEL USAGE HRS.	AVE. INLET TEMP	RUNNING TIME MINS.	DOWN TIME	AVG. WET MOISTURE	AVG. DRY MOISTURE	REASON FOR OIL USAGE
CORE	7720	0	1220	704	16	50.2%	5.0%	None here
SURFACE	8880	0	1160	704	16	46.0%	7.7%	None here

# OF UNITS	1/4	5/16	3/8	7/16	15/32	1/2	19/32	23/32	OTHER
A				112					
A 1/2 UNITS									
U				3 pcs					
E & X				48 pcs					

IF LESS THAN 99.5%, WHY?

**\*\*\*MAINTENANCE/LOCK-OUT LOG\*\*\***

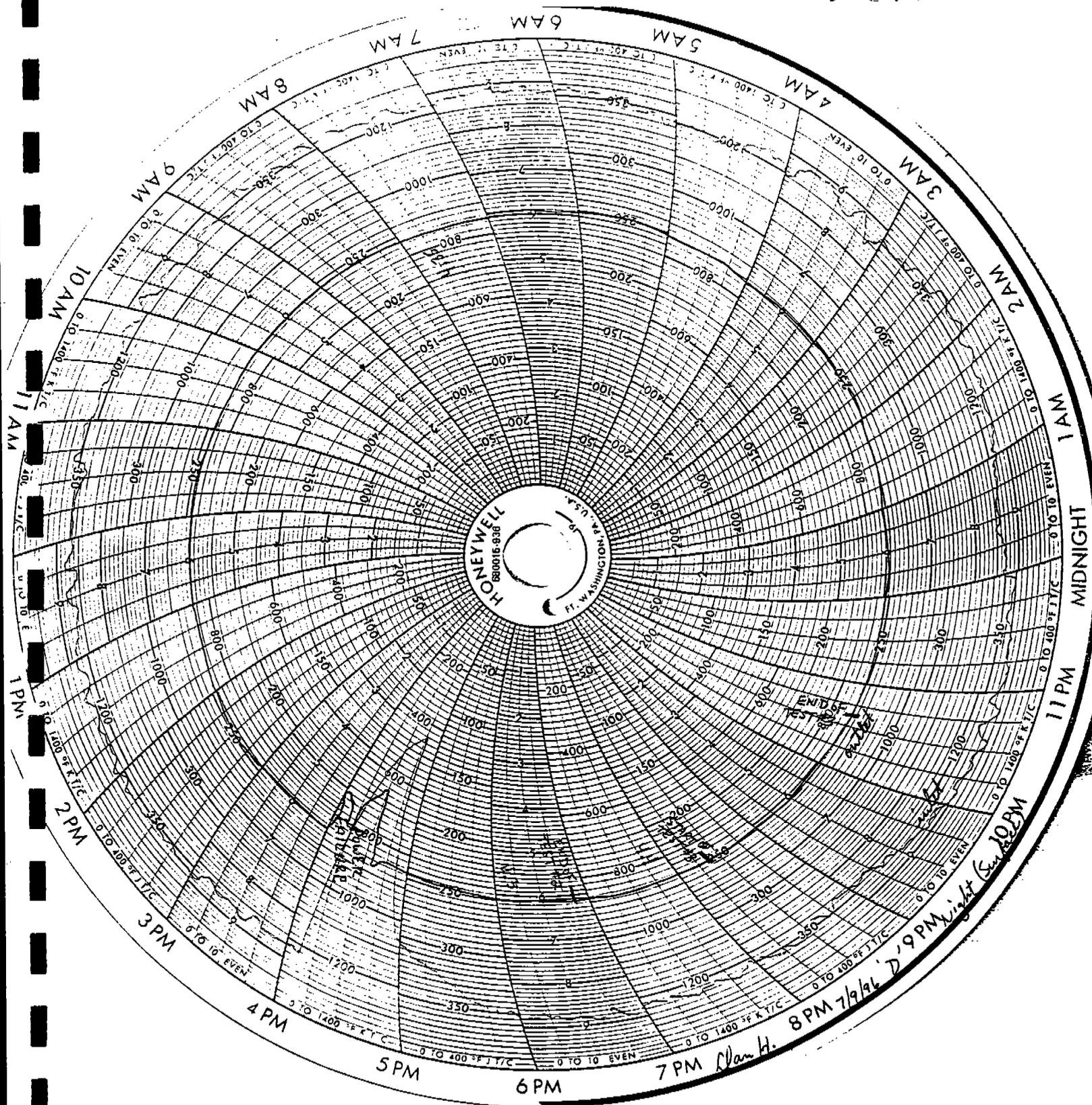
MOTOR #	LOCKED OUT	FROM	TO	BRIEF DESCRIPTION OF WORK BEING DONE	INITIALS OF PERSON LOCKING OUT

**PERSONNEL COMMENTS/CONCERNS:**

ABSENT/TARDY	REASON	EXTRA PERSONNEL	REASON



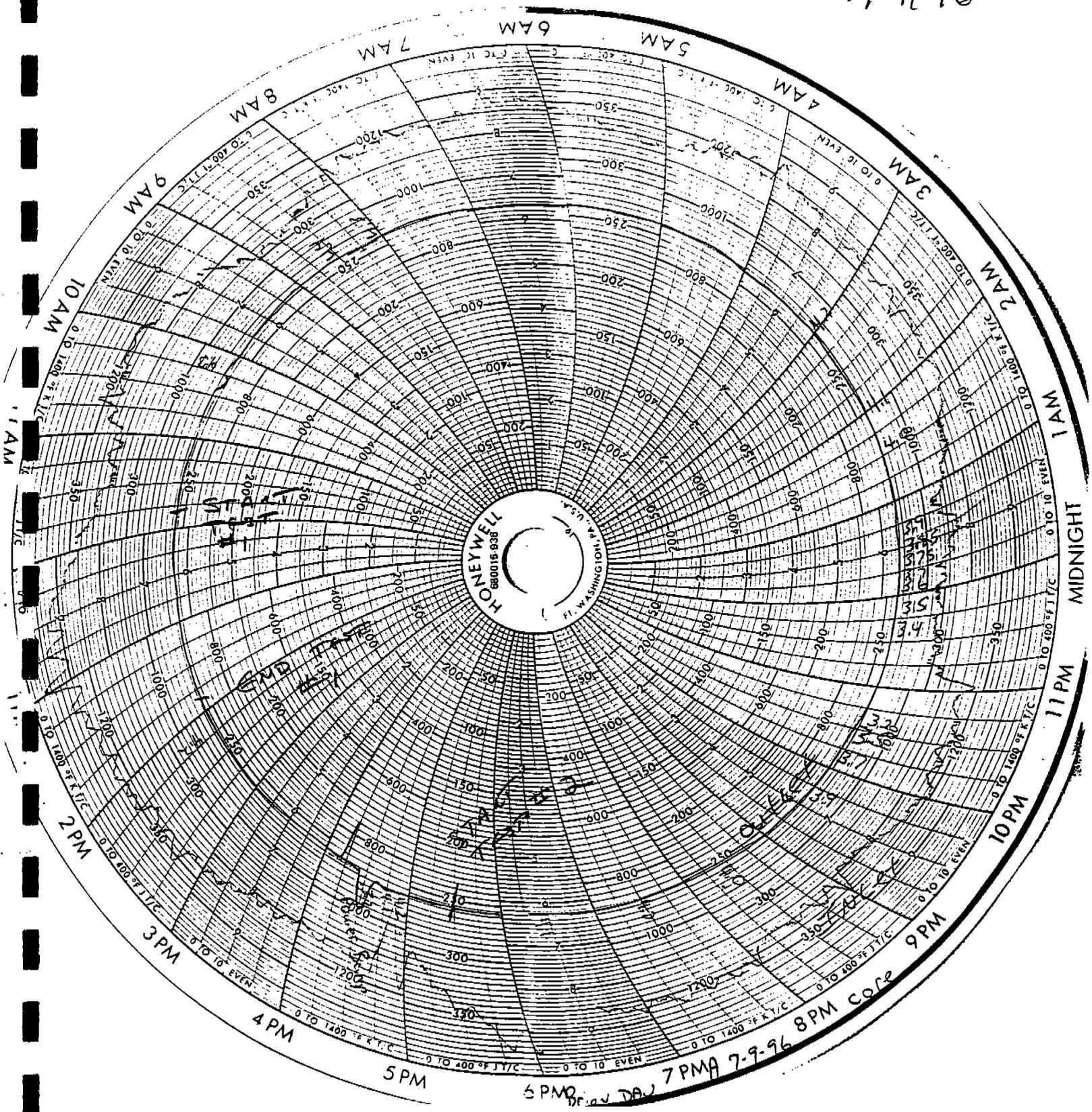
Houston  
SURFACE DRYER  
7/9/96



ENTIRE  
8/28/96  
8 PM 7/9/96 D'9 PM Night (5/10) 2 PM

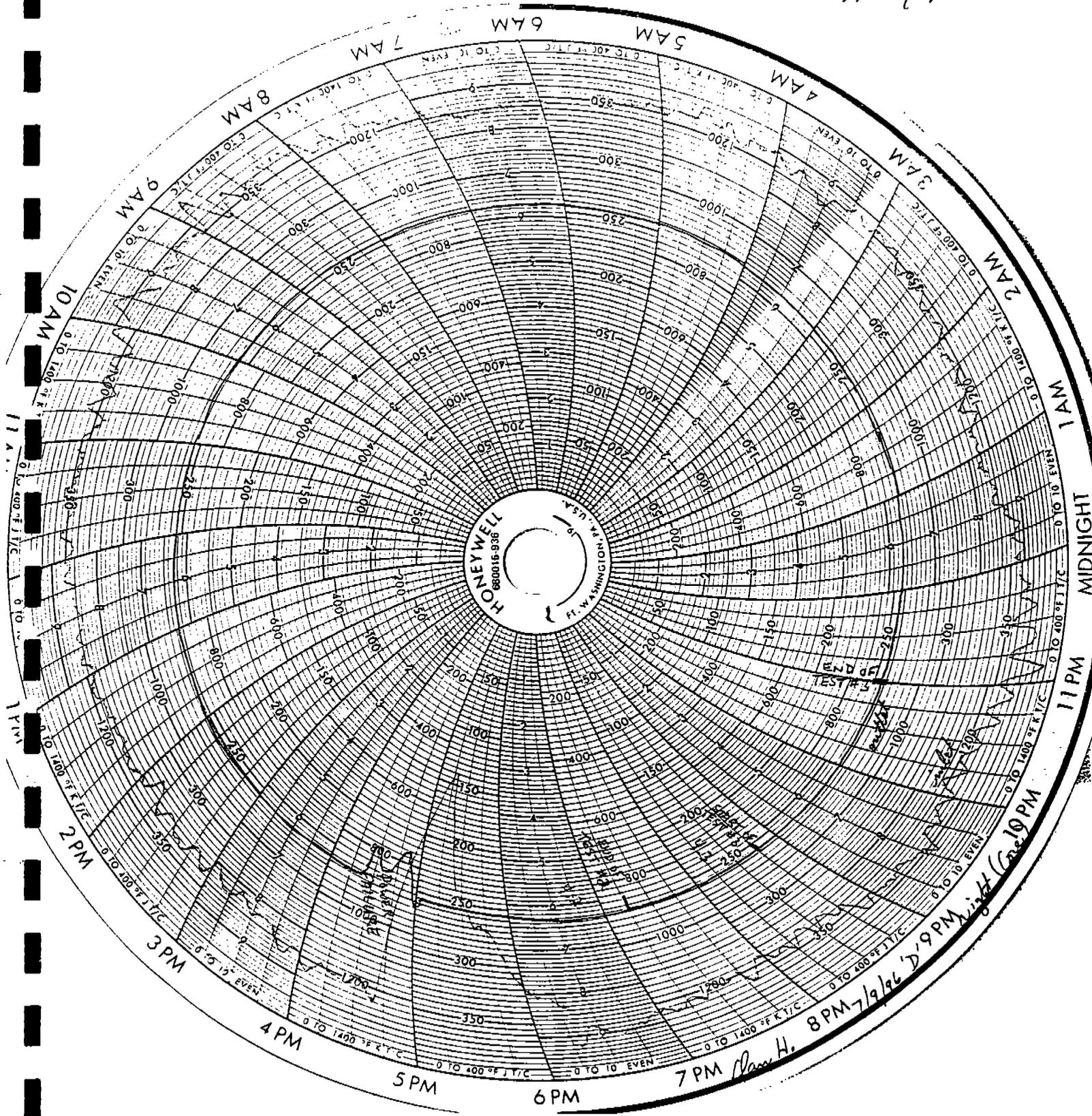
Van H.

Houston  
CORE DRYER  
7/9/96



5 PM  
6 PM  
7 PM  
8 PM  
9 PM  
10 PM  
11 PM  
MIDNIGHT  
1 AM  
2 AM  
3 AM  
4 AM  
5 AM  
6 AM  
7 AM  
8 AM  
9 AM  
10 AM  
11 AM

Houlton  
CORE DRYER  
7/9/96



Brain/force 7-9-96

DRYER READINGS - HOULTON

10 min TIME	FACE				CORE				WET BIN		CORE		WET BIN		CORE		FACE		EVERY HOUR FLAKE MOISTURE	
	OUT. SET POINT	FEED RATE	INLET TEMP	OUTLET TEMP	FUEL COUNT	WET BIN LEVEL	OUTLET TEMP	FEED RATE	INLET TEMP	OUTLET TEMP	FUEL COUNT	WET BIN LEVEL	FACE	LEVEL	FACE	LEVEL	IN	OUT	IN	OUT
8:00	242	4.3	1131	242.1	820	1/2+	262.8	4.0	1118	262.8	647	1/2+	3/1	3/1+	3/1+	43.4%	4.8%			
8:10	242	4.3	1132	242.2	986	1/2+	261.0	4.0	1166	261.0	822	1/2+	3/1	3/1+	3/1+					
8:20	242	4.1	1127	242.1	1046	1/2+	266.0	3.9	1193	266.0	931	1/2+	3/1	3/1+	3/1+					
8:30	243.5	4.1	1096	243.8	1198	1/2	261.3	3.9	1166	261.3	1016	1/2+	3/1	3/1+	3/1+					
8:40	245	3.8	1136	244.5	1316	1/2-	262.2	3.7	1173	262.2	1172	1/2-	3/1	3/1	3/1					
8:50	D R V E R					1/2	263.1	3.5	1155	263.1	1160	1/2	3/1	3/1	3/1					
9:00	D R V E R					1/2+	266	3.2	1043	265.4	1308	1/2+	3/1	3/1	3/1					
9:10	245	3.6	1019	245.0	1519	1/2+	266	3.2	1029	266.1	1396	1/2+	3/1	3/1+	3/1+					
9:20	245	3.8	1050	247.3	1663	1/2+	266	3.2	1040	266.1	1523	1/2+	1/2+	1/2+	1/2+					
9:30	245	3.9	1086	249.9	1774	1/2+	266.3	3.2	1040	266.1	1523	1/2+	1/2+	1/2+	1/2+					
9:40	245	4.0	1118	245.1	1896	3/4-	264.5	3.5	1052	264.5	1649	1/2+	1/2	1/2+	1/2+					
9:50	245	4.0	1140	245.1	1996	3/4-	263	3.6	1088	263.9	1710	3/4-	1/2	1/2	1/2					
10:00	244	4.1	1112	249.2	2113	3/4-	263	3.9	1065	263.4	1793	3/4-	1/2	1/2	1/2					
10:10	244	4.1	1104	243.9	2237	3/4+	263	3.9	1088	263.0	1878	3/4-	1/2	1/2	1/2					
10:20	244	4.1	1112	244.0	2360	3/4-	263	3.9	1132	262.9	1991	3/4-	1/2	1/2	1/2					
10:30	244	4.1	1112	244.1	2490	3/4	263	3.9	1135	263.0	2101	3/4-	1/2	1/2	1/2					
10:40	243	4.2	1143	243.4	2613	3/4	263	4.0	1159	263.0	2222	3/4	1/2	1/2	1/2					
10:50	243	4.2	1156	243.0	2734	3/4+	263	4.1	1168	263.2	2318	3/4	1/2	1/2	1/2					
11:00	243	4.2	1148	242.9	2861	1/2	263	4.1	1156	263.1	2418	1/2+	1/2	1/2	1/2					
11:10	243	4.2	1160	243.0	2990	1/2	263	4.1	1147	262.8	2522	1/2	1/2	1/2	1/2					
11:20	243	4.2	1188	243	3158	1/2	263	4.2	1172	262.6	2636	1/2	1/2	1/2	1/2					
11:30	243	4.2	1132	243.1	3268	1/2-	263	4.2	1170	262.5	2780	1/2	1/2	1/2	1/2					
11:40	243	4.2	1138	243.0	3381	1/2	263	4.2	1202	263.7	2885	1/2	1/2	1/2	1/2					
11:50	243	4.2	1141	243.1	3520	1/2	263	4.2	1152	262.9	2983	1/2+	1/2	1/2	1/2					
12:00	243	4.2	1127	243.0	3640	1/2	263	4.2	1138	262.9	3091	1/2+	1/2	1/2	1/2					
12:10	243	4.2	1117	243.1	3762	1/2	263	4.2	1153	263.1	3175	1/2+	1/2	1/2	1/2					
12:20	243	4.2	1107	242.8	3867	1/2	263	4.2	1176	263.0	3306	1/2+	1/2	1/2	1/2					
12:30	243	4.2	1149	242.8	4008	1/2	263	4.2	1203	262.8	3410	1/2	1/2	1/2	1/2					
12:40	243	4.2	1139	242.8	4134	1/2-	263	4.2	1217	263.3	3540	1/2	1/2	1/2	1/2					
12:50	243	4.2	1167	242.6	4270	1/2	263	4.2	1198	262.5	3661	1/2	1/2	1/2	1/2					
1:00	243	4.2	1195	243.2	4470	1/2+	263	4.2	1177	262.5	3761	1/2	1/2	1/2	1/2					
1:10	243	4.2	1169	243.0	4546	1/2+	263	4.2	1190	262.3	3885	1/2	1/2	1/2	1/2					
1:20	243	4.2	1111	243.0	4645	1/2+	263	4.2	1171	263.0	3998	1/2	1/2	1/2	1/2					
1:30	243	4.2	1102	243.0	4807	1/2+	263	4.2	1166	263.0	4091	1/2	1/2	1/2	1/2					
1:40	D R V E R					1/2-	263	4.2	1090	263.0	4221	1/2+	1/2	1/2	1/2					
1:50	243	4.2	856	246	4862	3/4-	263	4.2	1070	262.9	4353	1/2+	1/2	1/2	1/2					
2:00	247	4.0	812	243	4912	3/4-	263	4.4	1053	261.9	4397	3/4-	1/2	1/2	1/2					
									1444	262.2	4503	3/4-	1/2	1/2	1/2					





# DRYER OPERATING REPORT

OPERATOR Brian

CREW D

SHIFT DAY

DATE 7/9/96

## SURFACE DRYER

## CORE DRYER

TIME	INLET MOIST %	OUTPUT TEMP %	FEED SPEED	OUTLET MOIST CHAUS %	INLET TEMP %	DRY FUEL REV.	TIME EVERY HOUR	INLET MOIST %	OUTPUT TEMP %	FEED SPEED	OUTLET MOIST CHAUS %	INLET TEMP %	DRY FUEL REV.	HAMMER MILL LOAD %
7:00		241	4.45	8.0%	1130		7:00		259	4.4	4.4%	1200		35%
8:00		242	4.3	7.4%	1139	814	8:00		261	4.0	4.8%	1122	683	55%
9:00		Just started up				1387	9:00		266	3.2	4.4%	1034	1298	40%
10:00	47.8%	244	4.1	7.0%	1114	2096	10:00	43.4%	263	3.9	5.8%	1092	1871	45%
11:00		243	4.2	7.2%	1148	2874	11:00		263	4.1	5.2%	1165	2535	55%
12:00		243	4.2	8.0%	1123	3610	12:00		263	4.2	4.4%	1141	3177	50%
1:00		243	4.2	8.0%	1194	4381	1:00		263	4.2	4.8%	1189	3854	Full
2:00		<del>247</del>	<del>4.0</del>	<del>9.0%</del>	<del>912</del>	<del>4862</del>	2:00		262	4.4	4.2%	1190	4503	Full
3:00		243	4.4	6.6%	1082	5291	3:00		262	4.3	4.6%	1134	5132	35%
4:00		243	4.4	6.6%	1152	6140	4:00		262	4.3	4.6%	1248	5847	60%
5:00		243	4.4	7.0%	1157	6914	5:00		262	4.2	4.2%	1170	6518	40%
6:00		243	4.3	8.6%	1114	7720	6:00		262	4.2	4.2%	1149	7156	50%

10  
2

2

**COMMENTS AND REASONS FOR DOWNTIME:**

- 8<sup>47</sup> Surface dryer down, Dry bin full
- 8<sup>57</sup> Started surface dryer
- 9<sup>40</sup> Surface dryer down<sup>(3)</sup>, woodfuel flame went out,
- 9<sup>43</sup> Started surface on oil, run oil 41 minutes and then back on woodfuel
- 5<sup>40</sup> Both dryers down, Power Bump,
- 5<sup>42</sup> Both dryers running

# DRYER OPERATING REPORT

OPERATOR Dan H.

CREW D

SHIFT Night

DATE 7/9/96

## SURFACE DRYER

## CORE DRYER

TIME	INLET MOIST %	OUTPUT TEMP %	FEED SPEED	OUTLET MOIST CHAUS %	INLET TEMP %	DRY FUEL REV.	TIME EVERY HOUR	INLET MOIST %	OUTPUT TEMP %	FEED SPEED	OUTLET MOIST CHAUS %	INLET TEMP %	DRY FUEL REV.	HAMMER MILL LOAD %
7:00	46.0%	243	4.3	7.6%	1180	6	7:00	50.2%	262	4.2	5.2%	1210	0	60%
8:00		242	4.4	7.8%	1160	775	8:00		262	4.3	5.2%	1250	659	55%
9:00		242	4.4	7.0%	1190	1558	9:00		262	4.3	5.2%	1330	1323	50%
10:00		241	4.4	8.0%	1140	2434	10:00		262	4.3	4.4%	1160	2056	50%
11:00		241	4.4	7.2%	1170	3099	11:00		261	4.3	5.2%	1230	2628	Full
12:00		238	4.3	8.0%	1130	4137	12:00		261	4.3	6.8%	1220	3511	50%
1:00		238	4.3	8.2%	1170	4776	1:00		261	4.3	5.0%	1240	4059	55%
2:00		237	4.35	7.8%	1140	5708	2:00		261	4.3	4.8%	1290	4895	55%
3:00		237	4.35	7.6%	1160	6249	3:00		261	4.3	4.6%	1210	5364	50%
4:00		237	4.35	8.0%	1170	7060	4:00		261	4.3	4.2%	1160	6102	55%
5:00		237	4.35	7.6%	1170	7716	5:00		261	4.3	5.6%	1130	6665	55%
6:00	STARTING BACK UP (POWERBUMP)						6:00	STARTING BACK UP (POWERBUMP)						50%

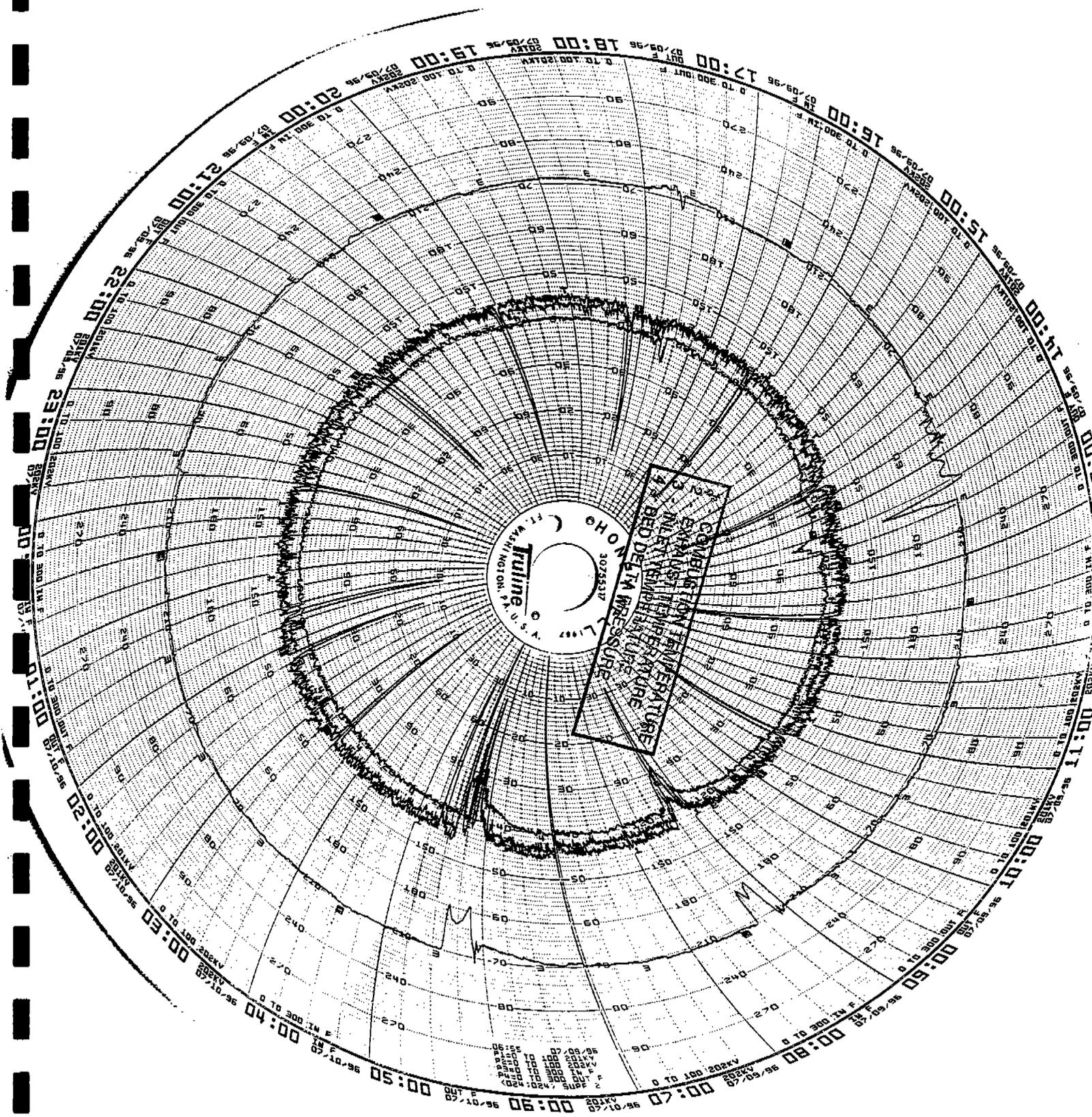
16

16

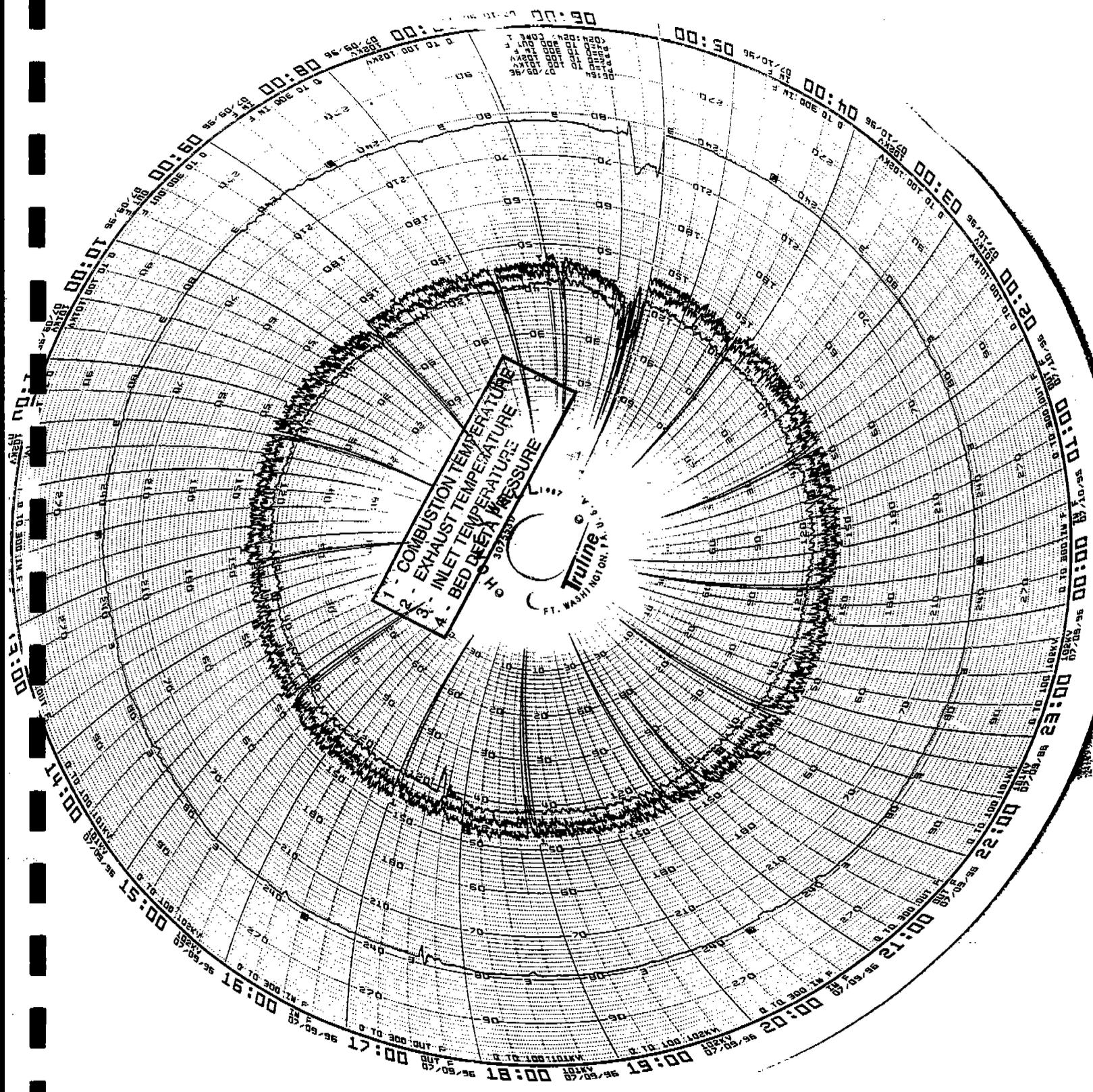
**COMMENTS AND REASONS FOR DOWNTIME:**

5:40 Powerbump, both dryers down.  
 5:50 Started both dryers.

Houlton 7/9/96  
SURFACE E-TUBE



Houston 7/9/96  
CORE - E - TUBE



E-tube Data Sheet  
Houlton, Maine

Operator Brent Carmichael

Date 7/9 / 1996

Time	Core Unit										Surface Unit											
	T/R Set #101					T/R Set #102					T/R Set #201					T/R Set #202						
	mA	Kv	Spk/ min	mA	Kv	Spk/ min	Quench Inlet	Quench Outlet	PRSS	mA	Kv	Spk/ min	Quench Inlet	Quench Outlet	PRSS	mA	Kv	Spk/ min	Quench Inlet	Quench Outlet	PRSS	Flush Time
10:00	280	47	14.9	150	47	15.0	8	27	200	46	14.9	180	46	14.9	25	180	46	14.9	10	25		
10:10	210	46	15.0	155	46	14.9	8	27	210	47	14.9	125	46	14.9	25	125	46	14.9	10	25		
10:20	270	44	14.8	170	46	14.9	8	27	195	47	14.9	160	46	14.9	24	160	46	14.9	10	24		
10:30	250	46	14.9	180	45	14.9	8	27	210	45	14.9	180	44	14.9	25	180	44	14.9	10	25		
10:40	285	46	14.9	155	43	14.9	8	27	190	44	15.0	190	42	14.9	25	190	42	14.9	10	25	10:48-Surface	
10:50	190	47	15.0	190	43	14.9	8	27	209	44	16.4	187	45	14.9	24	187	45	14.9	10	24		
11:00	220	47	15.0	200	44	14.9	8	27	200	45	14.7	184	45	14.8	25	184	45	14.8	10	25		
11:10	210	46	15.0	195	43	14.9	8	27	210	44	14.9	180	44	14.7	25	180	44	14.8	10	25		
11:20	220	45	14.9	160	42	14.9	8	27	195	46	14.8	190	43	14.9	25	190	43	14.9	10	25		
11:30	260	46	14.8	150	42	14.9	8	28	210	43	14.9	190	43	14.9	25	190	42	15.0	10	25	11:35-core	
11:40	210	45	15.0	190	43	16.3	8	27	225	44	15.0	170	44	15.0	25	170	40	14.9	10	25		
11:50	200	46	14.9	190	43	14.7	8	27	210	44	14.8	150	42	14.9	25	150	42	14.9	10	25		
12:00	230	45	15.0	195	43	15.0	8	27	225	43	14.7	195	43	14.9	25	195	40	14.9	10	25		
12:10	235	46	14.8	210	47	14.9	8	27	210	44	14.9	205	44	14.8	25	205	44	14.8	10	25		
12:20	240	47	14.9	170	42	15.0	8	27	230	45	14.7	200	44	15.0	25	200	44	15.0	10	25		
12:30	250	47	14.9	190	43	14.9	8	27	220	43	14.9	190	43	15.0	25	190	41	15.0	10	25		
12:40	270	47	14.9	165	44	15.0	8	27	190	43	14.9	130	43	17.1	25	130	43	17.1	10	25	12:42-Surface	
12:50	240	45	14.9	130	44	14.8	8	27	185	45	14.9	125	45	14.9	25	125	43	14.9	10	25		
1:00	245	46	14.9	190	43	14.9	8	27	220	43	14.9	195	43	14.9	25	195	43	14.9	10	25		
1:10	280	49	26.5	190	44	25.2	8	27	220	44	23.7	245	43	24.7	25	245	43	24.7	10	25		
1:20	260	47	24.7	180	43	24.9	8	27	240	45	24.9	220	44	24.8	25	220	44	24.8	10	25		
1:30	240	46	30.5	210	44	29.8	8	27	210	43	29.8	200	44	30.0	25	200	44	29.8	10	25	12:6-core	
1:40	260	47	29.8	200	44	29.8	8	27	245	43	29.8	200	42	29.9	25	200	42	29.9	10	25		
1:50	300	49	29.8	220	45	29.9	8	27	400	48	29.7	260	43	29.6	26	260	43	29.6	10	26		

AM

PM ↓

2

E-tube Data Sheet  
Houlton, Maine

Operator Brent Carmichael

Date 7/19 / 1996

Time	Core Unit										Surface Unit											
	T/R Set #101					T/R Set #102					T/R Set #201					T/R Set #202						
	mA	Kv	Spk/ min	mA	Kv	Spk/ min	Quench Inlet	Quench Outlet	mA	Kv	Spk/ min	mA	Kv	Spk/ min	Quench Inlet	Quench Outlet	mA	Kv	Spk/ min	Quench Inlet	Quench Outlet	Flush Time
2:00	260	48	29.9	170	43	30.0	8	27	360	43	29.9	320	43	29.8	10	25	320	43	29.8	10	25	
2:10	250	47	29.8	200	43	29.9	9	27	310	44	29.9	270	44	29.9	10	25	270	44	30.0	10	25	
2:20	235	48	29.8	260	43	29.8	8	27	340	46	29.6	340	45	29.9	10	25	340	45	29.9	10	25	
2:30	270	46	30.1	190	44	29.8	9	27	120	11	30.5	250	40	29.9	10	25	250	40	29.9	10	25	8:31 - surface
2:40	265	48	29.7	190	43	29.9	8	27	210	44	31.0	225	42	30.0	10	25	225	42	30.0	10	25	
2:50	300	49	29.8	185	42	29.8	8	27	240	46	29.8	260	42	29.8	10	25	260	42	29.8	10	25	
3:00	265	47	29.8	180	43	29.9	8	27	260	46	29.8	180	43	29.8	10	25	180	43	29.8	10	25	
3:10	270	46	29.8	230	43	30.0	9	27	240	43	29.9	250	42	29.9	10	25	250	42	29.9	10	25	3:15 code
3:20	280	48	30.0	240	45	30.8	9	27	240	45	29.8	200	43	29.8	10	25	200	43	29.8	10	25	TEST 315
3:30	285	47	29.9	260	44	29.9	9	27	225	44	29.9	190	42	29.9	10	25	190	42	29.9	10	25	
3:40	280	47	29.7	220	45	29.8	9	27	270	43	29.9	180	43	29.9	10	25	180	43	29.9	10	25	
3:50	240	46	30.0	220	44	29.9	8	27	210	45	29.8	190	45	29.8	10	25	190	45	29.8	10	25	
4:00	270	48	29.8	170	45	29.9	8	27	250	44	30.0	190	44	30.0	10	25	190	44	30.0	10	25	
4:10	255	49	29.9	160	45	29.8	9	27	280	45	29.8	180	42	29.8	10	25	180	42	29.8	10	25	TEST 1
4:20	260	47	29.7	220	46	29.8	8	27	220	44	29.8	240	47	29.9	10	25	240	47	29.9	10	25	4:24 surface
4:30	265	50	29.7	220	43	29.9	9	27	215	45	29.7	180	44	31.0	10	25	180	44	31.0	10	25	
4:40	260	48	30.0	215	43	29.8	8	27	230	44	29.9	180	43	29.9	10	25	180	43	29.9	10	25	
4:50	225	47	30.0	190	45	30.0	9	27	190	44	29.8	240	44	30.0	10	25	240	44	30.0	10	25	
5:00	250	46	29.7	210	44	29.8	8	27	240	44	29.8	210	43	29.8	10	25	210	43	29.8	10	25	
5:10	280	46	30.8	200	44	29.8	8	28	240	45	29.9	200	44	29.9	10	25	200	44	29.9	10	25	
5:20	260	48	30.0	200	46	30.0	8	27	240	46	29.8	200	44	29.8	10	25	200	44	29.8	10	25	
5:30	220	46	29.7	200	45	29.8	8	27	240	46	29.8	200	44	29.8	10	25	200	44	29.8	10	25	TEST 2 5:30
5:40	220	45	29.6	210	44	29.7	8	27	240	45	29.8	200	46	29.8	10	25	200	46	29.8	10	25	SKIN 0080
5:50	280	50	29.9	240	46	29.8	8	27	220	46	29.8	220	47	29.8	10	24	220	47	29.8	10	24	

PM

22

E-tube Data Sheet  
Houlton, Maine

JOE CHARENTE  
Operator Brent Coffman

Date 7/9/1996

Time	Core Unit										Surface Unit							
	T/R Set #101					T/R Set #102					T/R Set #201			T/R Set #202				
	mA	Kv	Spk/min	mA	Kv	Spk/min	Quench Inlet	Quench Outlet	Press	mA	Kv	Spk/min	mA	Kv	Spk/min	Quench Inlet	Quench Outlet	Flush Time
6:00	300	47	29.7	200	46	29.7	8	27		220	46	29.7	218	43	29.8	10	25	
6:10	290	50	29.7	220	46	29.7	8	27		230	44	30.0	240	46	29.8	10	25	
6:20	280	48	29.5	180	43	29.7	8	27		280	47	30.8	180	44	29.7	9	25	
6:30	260	50	29.8	170	46	29.8	8	27		240	47	29.9	200	45	29.9	9	25	
6:40	250	47	29.9	180	44	29.9	8	27		250	46	30.0	220	46	29.8	9	25	
6:50	260	47	29.8	220	46	29.8	8	27		200	44	29.8	200	44	29.8	9	25	658
7:06	280	50	30.1	170	42	31.8	9	27		200	45	29.9	260	46	29.9	10	25	
7:10	200	46	29.9	210	46	29.9	9	27		180	44	29.8	280	47	29.7	10	25	
7:50	280	50	29.8	230	47	29.8	9	27		260	48	29.7	240	48	29.8	10	25	
8:00	260	48	29.7	180	45	30.1	9	27		260	45	29.9	220	47	30.0	10	25	
8:10	260	48	29.8	210	46	30.0	9	27		250	44	29.8	200	46	29.8	10	25	
8:20	280	47	30.0	210	47	29.8	9	27		220	46	29.9	220	42	29.7	10	25	
8:30	250	50	29.8	200	46	28.9	9	27		250	47	30.0	200	44	29.9	10	25	
8:40	280	49	29.8	190	46	29.9	9	27		240	47	29.9	260	46	29.8	10	25	
8:50	280	48	30.0	200	47	29.8	9	27		260	48	29.8	220	44	29.8	10	25	
7:06	320	49	31.8	200	46	29.8	9	27		280	49	29.9	200	43	29.8	10	25	

TEST 2  
6:15 PM

COIL  
7:10

805 - SURF

PM

23

E-tube Data Sheet  
Houlton, Maine

Operator Brian/Lance

Date 7/9/1996

10  
min

Time	Core Unit										Surface Unit						
	T/R Set #101					T/R Set #102					T/R Set #202						
	mA	Kv	Spk/ min	mA	Kv	Spk/ min	Quench Inlet	Quench Outlet	mA	Kv	Spk/ min	mA	Kv	Spk/ min	Quench Inlet	Quench Outlet	Flush Time
8:00							8	28							9	24	
8:10							8	28							9	24	
8:20							8	28							9	24	
8:30							8	28							9	24	
8:40							7	28							9	25	
8:50							8	29							9	25	
9:00							8	28							9	24	
9:10							8	28							9	24	
9:20							8	28							9	24	
9:30							8	28							9	24	
9:40							8	28							9	24	
9:50							8	28							9	24	
10:00							8	28							9	24	
10:10							8	28							9	24	
10:20							8	28							9	24	
10:30							8	28							9	24	
10:40							8	28							9	24	
10:50							8	28							9	24	
11:00							8	28							9	24	
11:10							8	28							9	24	
11:20							8	28							9	24	
11:30							8	28							9	24	
11:40							8	28							9	24	
11:50							8	28							9	24	

# E-tube Data Sheet

Houlton, Maine

Operator Brian/Leah

Date 7/9/1996

Time	Core Unit						Surface Unit						
	T/R Set #101			T/R Set #102			T/R Set #201			T/R Set #202			
	mA	Kv	Spk/min	mA	Kv	Spk/min	Quench Inlet	Quench Outlet	mA	Kv	Spk/min	Quench Inlet	Quench Outlet
12:00							8	28				9	24
12:10							8	28				9	24
12:20							8	28				9	24
12:30							8	28				9	24
12:40							8	28				9	24
12:50							8	28				9	24
1:00							8	28				9	24
1:10							8	28				9	24
1:20							8	28				9	24
1:30							8	28				9	24
1:40							8	28				9	24
1:50							8	28				9	24
2:00							8	28				9	24
2:10							8	28				9	24
2:20							8	28				9	24
2:30							8	28				9	24
2:40							8	28				9	24
2:50							8	28				9	24
3:00							8	28				9	24
3:10							8	28				9	24
3:20							8	28				9	24
3:30							8	28				9	24
3:40							8	28				9	24
3:50							8	28				9	24

250  
5/10/96

E-tube Data Sheet  
Houlton, Maine

Operator Peter/Lance

Date 7/9/1996

Time	Core Unit						Surface Unit							
	T/R Set #101			T/R Set #102 Pres			T/R Set #201			T/R Set #202				
	mA	Kv	Spk/min	mA	Kv	Spk/min	Quench Inlet	Quench Outlet	mA	Kv	Spk/min	Quench Inlet	Quench Outlet	Flush Time
4:00							8	28				9	24	
4:10							8	28				9	24	
4:20							8	28				9	24	
4:30							8	28				9	24	
4:40							8	28				9	24	
4:50							8	28				9	24	
5:00							8	28				9	24	
5:10							8	28				9	24	
5:20							8	28				9	24	
5:30							8	28				9	24	
5:40							8	28				9	24	
5:50							8	28				9	24	
6:00							8	28				9	24	
6:10							8	28				9	24	
6:20							8	28				9	24	
6:30							8	28				9	24	
6:40							8	28				9	24	
6:50							8	28				9	24	
7:00							8	28				9	24	
7:10							8	28				9	24	
7:20							8	28				9	24	
7:30							8	28				9	24	
7:40							8	28				9	24	
7:50							8	28				9	24	

5:40-5:50

5:20-5:30

5:40-5:50

6:20-6:30



E-tube Data Sheet  
Houlton, Maine

Operator B. 150/Lease

Date 7/9/1996

10  
min.

Time	Core Unit						Surface Unit							
	T/R Set #101			T/R Set #102 T e m p.			T/R Set #201			T/R Set #202 T e m p.				
	mA	Kv	Spk/ min	mA	Kv	Spk/ min	Quench Inlet	Quench Outlet	mA	Kv	Spk/ min	Quench Inlet	Quench Outlet	Flush Time
8:00							227	164				222	148	
8:10							227	167				222	143	
8:20							229	168				222	148	
8:30							229	165				222	147	
8:40							231	162				201	113	
8:50							232	163				221	134	
9:00							232	162				220	141	
9:10							232	161				220	140	
9:20							232	162				220	141	
9:30							231	164				221	144	
9:40							231	162				221	147	
9:50							230	163				222	148	
10:00							230	164				222	147	
10:10							230	165				222	146	
10:20							231	165				221	147	
10:30							230	166				222	148	
10:40							229	167				222	148	
10:50							230	167				222	150	
11:00							230	168				223	148	
11:10							230	167				223	148	
11:20							231	169				222	149	
11:30							230	165				223	147	
11:40							230	167				223	148	
11:50							230	167				222	150	
11:54							230	166				222	150	

E-tube Data Sheet  
Houlton, Maine

Operator Brian/Lance

Date 7/19 / 1996

Time	Core Unit						Surface Unit							
	T/R Set #101			T/R Set #102 Temp			T/R Set #201			T/R Set #202 Temp				
	mA	Kv	Spk/ min	mA	Kv	Spk/ min	Quench Inlet	Quench Outlet	mA	Kv	Spk/ min	Quench Inlet	Quench Outlet	Flush Time
12:00							231	166				222	148	
12:10							231	167				221	147	
12:20							231	171				221	148	
12:30							231	168				220	150	
12:40							231	168				220	148	
12:50							231	167				220	150	
1:00							229	167				222	150	
1:10							229	164				221	146	
1:20							228	164				221	147	
1:30							228	164				220	147	
1:40							228	162				222	148	
1:50							229	164				213	141	
2:00							229	166				217	142	
2:10							229	168				213	143	
2:20							229	169				216	142	
2:30							230	166				219	141	
2:40							229	165				220	149	
2:50							229	165				221	148	
3:00							229	166				221	147	
3:10							229	166				222	150	
3:20							238	168				222	150	
3:30							231	172				222	150	
3:40							230	173				222	151	
3:50							230	166				222	152	

3:10 X  
3:15 X

E-tube Data Sheet  
Houlton, Maine

Operator Brian Leve

Date 7/19/1996

Time	Core Unit										Surface Unit				
	T/R Set #101					T/R Set #102					T/R Set #202				
	mA	Kv	Spk/min	mA	Kv	Spk/min	Quench Inlet	Quench Outlet	mA	Kv	Spk/min	Quench Inlet	Quench Outlet	Flush Time	
3:00							220	170				225	154		
4:10							229	169				223	153		
4:30							228	167				223	151		
4:50							229	168				219	149		
5:00							229	167				219	149		
5:10							229	167				219	149		
5:20							226	165				222	149		
5:30							228	168				223	153		
5:40							Power	Bump				Power	Bump		
5:50							229	166				224	147		
6:00							229	167				229	146		
6:10							230	171				223	147		
6:20							230	172				222	148		
6:30							230	173				223	149		
6:40							229	171				223	150		
6:50							230	169				224	151		
7:00							230	170				224	151		
7:10							230	170				223	150		
7:20							231	169				223	150		
7:30							230	169				223	151		
7:40							230	171				221	147		
7:50							230	171				222	148		

End  
Start #2  
5:13:5  
6:00  
Start #2  
6:19  
7:29  
7:29  
7:51  
Start #2



# E-TUBE LOGSHEET

L.P., HOULTON, MAINE

AM OPERATOR \_\_\_\_\_

PM OPERATOR SD

DATE 7/9/86

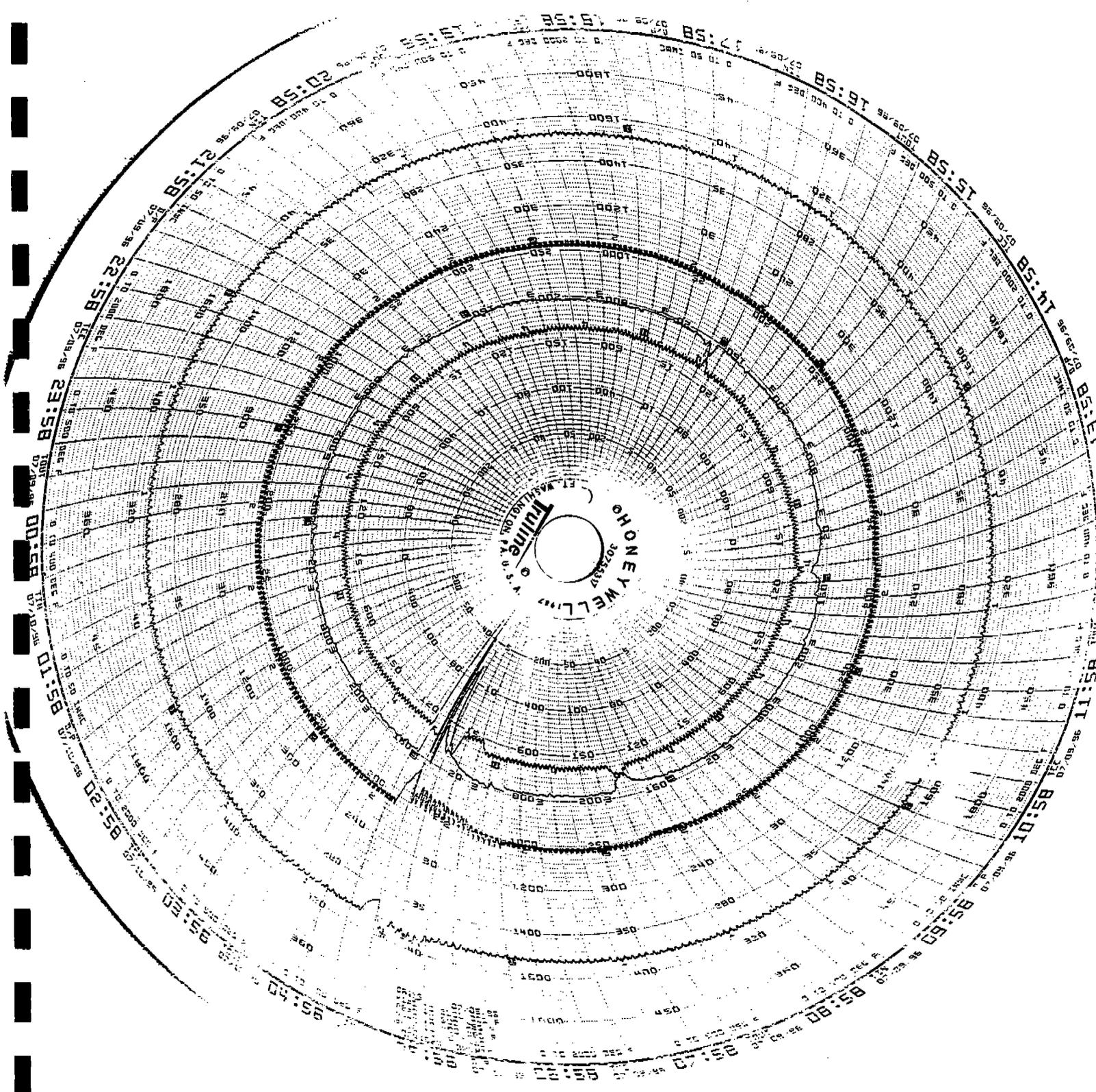
Time	T/R Control Panel Readings										Zycom				Begin / End of Shift Reading		
	Core Unit					Mesh Pad	Quench		Inlet Press in H2O		Outlet Press in H2O	Delta Press in H2O	Flush Water Gal	Make up Water Gal			
	T/R Set # 101	T/R Set # 102	T/R Set # 102				Inlet Temp	Outlet Temp	Inlet Press	Outlet Press							
mA	Kv	Spk/m	mA	Kv	Spk/m	Temp	Temp	in H2O	in H2O								
7	280	45	15.0	150	40	14.9	205	215	8	29	20						
11	290	50															
3																	
7																	
11	290	50	29.9	260	45	29.7	228	170	8	28							
3	240	45	29.8	160	45	29.8	229	169	8	28							

Time	Surface Unit										Zycom				Begin / End of Shift Reading		
	T/R Set # 201					Mesh Pad	Quench		Inlet Press in H2O		Outlet Press in H2O	Delta Press in H2O	Flush Water Gal	Make up Water Gal			
	T/R Set # 201	T/R Set # 202	T/R Set # 202				Inlet Temp	Outlet Temp	Inlet Press	Outlet Press							
mA	Kv	Spk/m	mA	Kv	Spk/m	Temp	Temp	in H2O	in H2O								
7	150	43	14.8	180	43	14.9	228	205	9	24	14						
11																	
3																	
7																	
11	220	45	27.8	200	45	27.8	218	150	9	24							
3	220	45	29.9	220	45	29.7	220	149	9	24							

Sample Times:	
Recycle Water % Solids:	
pH	
Recycle Blowdown Gallons:	

Caustic	
End:	
Start:	
Total:	
Defoamer	

Houlton Dryer RTO  
7/9/96



9.1  
B6.39 = GAL

RTO DATA SHEET  
HOULTON, MAINE

Operator Brent Carmichael

Press RTO

Dryer RTO X

Date 7/19/1996

Time	RTO CHAMBER BEDS							P-V			BURNERS			Δ		
	#1	#2	#3	#4	#5	#6	#7	Inlet Press	Burn #1	Burn #2	Burn #3	Inlet temp	Exh temp	Comb Temp	Press Drop	Gas meter
10:00	369	344	392	405	393	361	385	1.1	1515	1518	1518	151	238	1521	16	650327
10:10	368	343	397	405	391	363	387	0.9	1498	1505	1505	151	243	1523	15	650404
10:20	369	346	393	402	394	363	385	1.0	1531	1516	1508	151	243	1521	15	650488
10:30	369	344	398	406	392	364	388	1.0	1496	1504	1506	151	242	1526	15	650472
10:40	369	346	394	402	395	364	386	1.0	1531	1517	1507	152	248	1529	16	650549
10:50	368	344	399	403	392	365	388	1.1	1498	1511	1507	153	250	1520	15	650582
11:00	368	344	399	404	392	365	388	1.0	1498	1509	1506	153	249	1524	15	650621
11:10	369	345	399	403	393	365	388	1.0	1499	1511	1506	153	248	1523	15	650673
11:20	370	347	394	403	395	365	388	1.0	1526	1518	1509	153	245	1526	16	650761
11:30	370	346	399	402	393	366	388	1.1	1497	1511	1506	152	250	1523	15	650789
11:40	371	347	393	405	396	364	388	1.1	1522	1519	1513	152	242	1526	15	650869
11:50	371	345	399	405	393	365	390	0.9	1448	1504	1506	153	246	1524	16	650893
12:00	370	347	394	403	396	364	388	0.9	1532	1518	1509	153	249	1530	15	650929
12:10	370	345	399	404	393	365	390	0.9	1499	1504	1508	152	243	1531	15	650977
12:20	370	345	398	406	393	365	390	1.0	1508	1516	1519	153	246	1531	16	651050
12:30	370	346	399	402	394	366	389	1.0	1512	1509	1507	154	252	1522	16	651084
12:40	371	346	397	407	394	364	391	0.9	1499	1501	1514	153	243	1520	15	651139
12:50	371	348	395	402	396	365	388	1.0	1499	1513	1508	154	244	1524	15	651225
1:00	372	347	393	406	397	364	390	0.9	1509	1514	1518	154	242	1517	16	651224
1:10	370	348	398	401	396	366	389	1.0	1509	1510	1506	153	253	1520	16	651249
1:20	372	347	395	409	396	363	390	1.0	1510	1512	1517	151	242	1515	15	651318
1:30	369	347	398	401	395	365	389	1.0	1509	1506	1508	152	252	1518	16	651323
1:40	371	346	395	409	394	362	390	1.0	<del>1498</del>	1498	1511	145	241	1516	16	651445
1:50	369	346	397	400	394	364	388	0.9	1498	1507	1506	146	239	1515	16	651464
2:00	368	344	397	403	392	362	388	0.9	1497	1507	1506	150	245	1524	15	651528
2:10	368	346	393	400	394	362	386	1.1	1529	1514	1509	151	248	1529	16	651529
2:20	370	344	394	407	393	361	389	1.0	1499	1504	1517	152	241	1512	16	651689
2:30	370	345	392	405	395	361	388	1.1	1521	1516	1511	150	242	1521	16	651629

AM

↓ PM

W

# RTO DATA SHEET

## HOULTON, MAINE

Operator Brent Carmichael

Press RTO

Dryer RTO

Date 7/19/1996

Time	RTO CHAMBER BEDS							P-V				BURNERS				Inlet temp	Exh temp	Comb Temp	Press Drop	Gas meter
	#1	#2	#3	#4	#5	#6	#7	Inlet Press	Burn #1	Burn #2	Burn #3									
2:40	370	344	396	406	393	361	389	1.0	1499	1500	1511	1520	1520	241	1520	1520	15	657285		
2:50	370	345	391	405	395	361	388	1.0	1521	1515	1512	1521	1521	243	1521	1521	16	657289		
3:00	370	344	396	407	393	361	390	1.0	1500	1508	1515	1521	1521	242	1515	1515	16	657143		
3:10	370	346	394	402	395	363	388	1.1	1529	1513	1508	1524	1524	250	1524	1524	16	657832		
3:20	371	345	394	407	394	361	388	1.1	1515	1516	1515	1523	1523	243	1523	1523	16	6519045		
3:30	371	346	394	405	396	362	389	1.0	1526	1519	1511	1526	1526	246	1526	1526	16	6519111		
3:40	370	346	401	403	394	365	392	0.9	1497	1510	1507	1526	1526	250	1526	1526	16	652008		
3:50	372	348	396	407	396	364	391	1.1	1522	1516	1511	1522	1522	246	1522	1522	16	6520542		
4:00	371	347	402	404	394	366	391	1.0	1508	1511	1509	1521	1521	254	1521	1521	16	652059		
4:10	373	348	396	409	396	364	392	1.1	1518	1517	1514	1518	1518	243	1518	1518	16	652044		
4:20	372	348	401	403	395	366	392	0.9	1498	1502	1507	1518	1518	244	1518	1518	16	6521447		
4:30	372	347	401	405	395	365	393	0.9	1497	1509	1506	1527	1527	250	1527	1527	16	6522522		
4:40	371	348	399	401	396	366	391	1.0	1512	1511	1507	1522	1522	252	1522	1522	16	6522412		
4:50	373	349	399	409	394	364	393	0.9	1501	1502	1515	1513	1513	243	1513	1513	16	6523527		
5:00	371	348	399	401	395	365	391	1.0	1504	1513	1508	1523	1523	254	1523	1523	16	6523825		
5:10	372	348	395	405	396	364	390	1.0	1521	1511	1509	1525	1525	254	1525	1525	16	6524464		
5:20	372	347	398	408	395	363	392	1.0	1511	1513	1513	1527	1527	248	1527	1527	16	6524906		
5:30	373	348	394	405	397	363	390	1.1	1523	1520	1507	1522	1522	254	1522	1522	16	6525427		
5:40	371	349	397	401	396	365	390	0.9	1499	1509	1507	1524	1524	249	1524	1524	17	6525999		
5:50	370	348	399	400	395	366	391	0.8	1497	1505	1505	1511	1511	243	1511	1511	16	6526374		
6:00	370	347	397	406	395	364	389	0.9	1499	1502	1513	1514	1514	246	1514	1514	16	6526851		
6:10	371	349	398	401	394	363	391	1.1	1499	1501	1511	1521	1521	241	1521	1521	16	6527492		
6:20	370	348	399	400	395	365	390	0.9	1501	1505	1515	1521	1521	242	1521	1521	16	6528070		
6:30	371	348	396	402	395	365	389	1.0	1507	1506	1508	1514	1514	252	1514	1514	16	6528400		
6:40	371	349	395	403	396	364	390	1.0	1510	1508	1505	1520	1520	251	1520	1520	16	6528910		
6:50	373	348	396	406	396	365	391	1.0	1523	1510	1508	1521	1521	254	1521	1521	16	6529294		
7:00	371	348	400	401	395	367	391	1.0	1496	1509	1507	1523	1523	248	1523	1523	16	6529771		
7:10	373	347	399	407	395	365	393	1.0	1530	1517	1507	1523	1523	251	1523	1523	16	6530142		

PM

WS



# RTO LOGSHEET

Press \_\_\_\_\_

HOULTON, MAINE

Dryer

AM OPERATOR J. CHARETTE

PM OPERATOR S.D.

DATE 7 / 9 / 96

	7	11	3	7	11	3
BURNER #1 SETPOINT	1535 <sup>10</sup>	1535	1535	1535	1535	1535
BURNER #1 TEMP	1525		1520		1520	1512
BURNER #1 OUTPUT	30.5		31.3		31.3	31.0
BURNER #2 SETPOINT	1535 <sup>10</sup>	1535	1535	1535	1535	1535
BURNER #2 TEMP	1513		1499		1499	1510
BURNER #2 OUTPUT	14.5		25.2		25.2	14.3
BURNER #3 SETPOINT	1535 <sup>10</sup>	1535	1535	1535	1535	1535
BURNER #3 TEMP	1507		1510		1510	1506
BURNER #3 OUTPUT	42.4		36.6		36.6	41.7
INLET TEMP	151				155	153
CHAMBER TEMP	1524				1525	1520
EXHAUST TEMP	247				244	251
INLET PRESS	1.0				1.1	1.1
DELTA PRESS	16				16	16
VFD #1 AMPS	365				350	350
VFD #1 RPM	1365				1339	1346
VFD #2 AMPS	360				340	358
VFD #2 RPM	1366				1335	1343
P/V SETPOINT	1.0				1.0	1.0
P/V OUTPUT	66.0				65.1	67.5
RECOV CH 1 TEMP	374				374	371
RECOV CH 2 TEMP	345				349	347
RECOV CH 3 TEMP	396				397	403
RECOV CH 4 TEMP	410				409	412
RECOV CH 5 TEMP	394				397	395
RECOV CH 6 TEMP	363				365	361
RECOV CH 7 TEMP	387				392	390
FAN #1 SHAFT BRG	92				82	94
FAN #1 FAN BRG	103				98	112
FAN #2 SHAFT BRG	90				82	91
FAN #2 FAN BRG	88				88	84
PURGE FAN RUNNING	yes				yes	yes
BTUE SYSTEM ON	No	No	No	No	No	No
RTO GAS INLET PRESS	8					
VAPORIZ WATER TEMP						
VAPORIZ INLET PRESS						
VAPORIZ OUTLET PRE						
GAS METER READING						

(Last day of the Month)

RTO OPERATOR'S LOG #1

HOULTON, ME.

Date: 7-9-96

Shift Electrician inspect the RTO outside and take the following readings every two hours. Press Lineman to fill in when Electrician is busy.

DataLiner:

	Recovery Chamber Temperatures					Inlet Press. W.C.	Inlet Temp	Comb. Chamber Temp.	Exh. Temp.
	1	2	3	4	5				
M	341	328	343	350	342	4.4	123	1537	237
2	346	332	345	355	343	4.3	126	1549	238
3	348	337	346	361	344	4.2	128	1550	241
M	348	333	353	347	349	4.3	128	1552	239
1	344	336	346	352	351	4.4	126	1548	235
3	341	334	346	350	350	4.1	125	1524	231

ny Shift (at 12 AM): Propane tank #1 72 % Tank #2 64 %

og startup/shutdown times, problems, maintenance items, etc.:  
(use chartrecorder time)

RTO OPERATOR'S LOG #2

HOULTON, ME.

Date: 7-9-96

Shift Electrician inspect the RTO outside and take the following readings every FOUR hours. Press Lineman to fill in when Electrician is busy. Propane readings: 3 X per shift, Vaporizer: 1 X per shift.

RTO Delta P	Press. Inlet Duct	Burner				Motor Amps	Propane		Temperature Vaporizer
		Temperature #1	Temperature #2	Output % #1	Output % #2		Pressures RTO	Vaporizer In Out	

M	17	4.5	1549	1552	9.0	1.1	113	7	90	8	135
2	18	4.3	1544	1552	2.0	0	108				
3	18	4.1	1532	1545	14.0	0	113				
M	17	4.3	1529	1531	42.2	5.6	111	7	120	8	134
1	17	4.2	1549	1554	0.4	2.2	111				
3	17	4.1	1528	1533	3.6	0.4	111				

Burner Setpoints: 1) 1535

BTUE SYSTEM: ON  OFF

2) 1535

Readings taken by: DAY S. Traw

NITE S. D.

HOULTON BOARD WEIGHTS  
 (lbs./8x16 panel every 25th mat during test Times)  
 APPROXIMATE TIMES

7/16"		07/10/96	
KG	LBS	KG	LBS
90.80	200.21	85.70	188.97
90.60	199.77	90.70	199.99
79.10	174.42	90.10	198.67
92.10	203.08	89.30	196.91
92.40	203.74	88.10	194.26
85.90	189.41	89.10	196.47
90.50	199.55	90.60	199.77
93.00	205.07	92.90	204.84
94.10	207.49	88.60	195.36
91.30	201.32	89.50	197.35
89.00	196.25	92.90	204.84
<u>89.00</u>	<u>196.25</u>	<u>92.50</u>	<u>203.96</u>
88.10	194.26	90.60	199.77
88.90	196.02	90.10	198.67
91.60	201.98	90.30	199.11
91.60	201.98	91.70	202.20
90.40	199.33	90.30	199.11
87.20	192.28	90.90	200.43
88.60	195.36	93.10	205.29
86.50	190.73	94.10	207.49
89.60	197.57	91.10	200.88
88.90	196.02	93.20	205.51
89.40	197.13	93.10	205.29
89.90	198.23	93.00	205.07
89.70	197.79	93.50	206.17
90.30	199.11	93.70	206.61
86.80	191.39	91.80	202.42
93.30	205.73	94.40	208.15
89.50	197.35	93.50	206.17
93.60	206.39	93.20	205.51
92.70	204.40	88.40	194.92
93.10	205.29	90.30	199.11
91.10	200.88	90.00	198.45
92.40	203.74	89.80	198.01
93.80	206.83	92.20	203.30
100.10	220.72	89.90	198.23
96.90	213.66	92.10	203.08
95.60	210.80	92.90	204.84
96.40	212.56	93.50	206.17
95.00	209.48	90.20	198.89
93.70	206.61	91.30	201.32
98.00	216.09	94.10	207.49
94.80	209.03	94.30	207.93
95.60	210.80	92.30	203.52
92.80	204.62	91.60	201.98
91.90	202.64		0.00
92.80	204.62		0.00
90.20	198.89		0.00
91.30	201.32		0.00
	<b>201.5955</b>		<b>201.6105</b>
7% TRIM		7% TRIM	
8x16 WT.	187.48	8x16 WT.	187.50
4x8 NET	46.87	4x8 NET	46.87

## AIR POLLUTION SOURCE and CONTROL EQUIPMENT LOGSHEET

Operator DAN H. Crew D AM PM Date 7/9/96

Log the start/stop, (open/shut) times of the following Sources & Control Equipment. Use the time displayed on the telephone.

Sources: Forming Line, Dryers, Thermal Oil Heaters, RTO's,  
RTO Bypass Stack Damper (open/shut).

Control Equipment: ESP's, E-tubes, RTO's (Press/Dryer), &  
Baghouses

<u>Time</u>	<u>Item</u>	<u>Operation</u>	<u>Comment</u>
5:40 <sup>Am</sup>	Lost ALL POWER	stop	Everything Down
5:44 <sup>Am</sup>	#2 E.S.P. + #2 Korus	start	Power is back
5:46 <sup>Am</sup>	Baghouse	start	" " "
5:50 <sup>Am</sup>	E-Tubes (Both)	start	" " "
5:56 <sup>Am</sup>	R.T.O.	start	" " "
5:56 <sup>Am</sup>	Both dryers	start	" " "

Use Reverse side for additional space.

# AIR POLLUTION SOURCE and CONTROL EQUIPMENT LOGSHEET

Operator Brian Crew A (AM) PM Date 7-9-96

Log the start/stop, (open/shut) times of the following Sources & Control Equipment. Use the time displayed on the telephone.

Sources: Forming Line, Dryers, Thermal Oil Heaters, RTO's,  
RTO Bypass Stack Damper (open/shut).

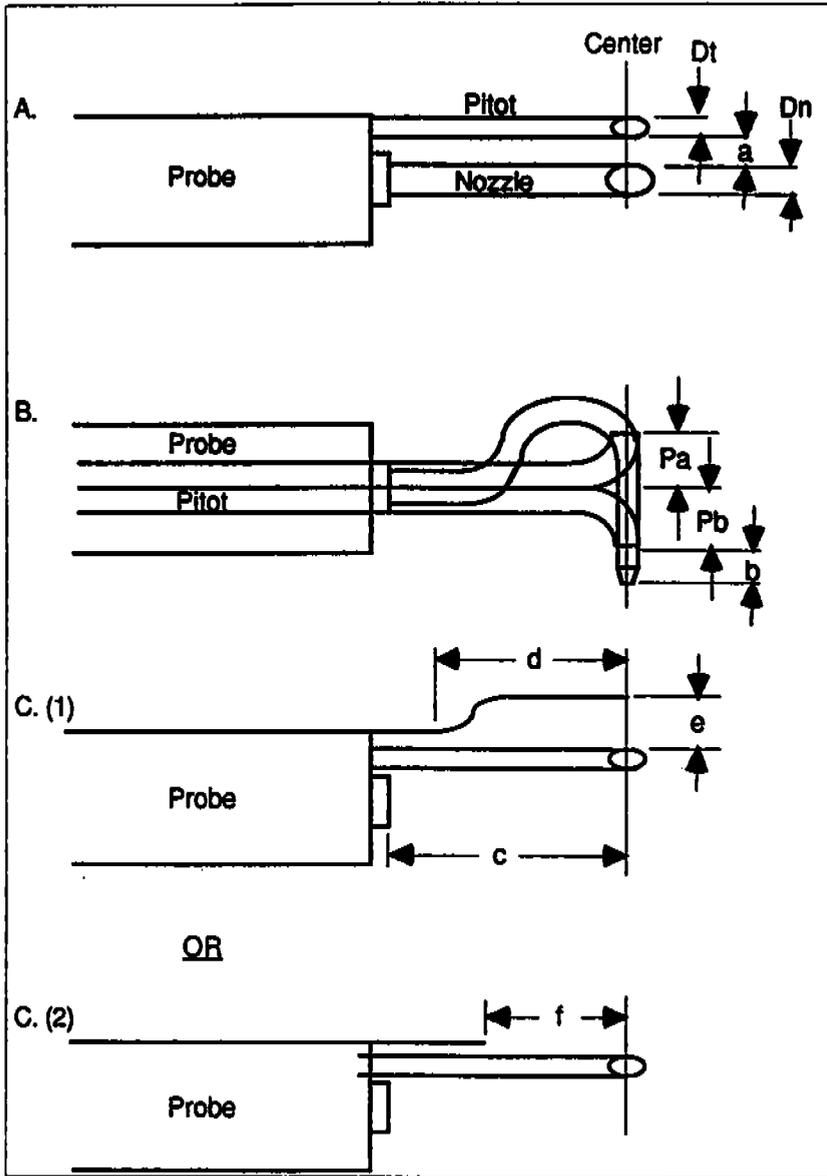
Control Equipment: ESP's, E-tubes, RTO's (Press/Dryer), &  
Baghouses

<u>Time</u>	<u>Item</u>	<u>Operation</u>	<u>Comment</u>
<u>847</u>	<u>SL dryer</u>	<u>STOP</u>	<u>Dry bin Full</u>
<u>857</u>	<u>SL dryer</u>	<u>Start</u>	
<u>140</u>	<u>SL dryer</u>	<u>stop</u>	<u>Woodfuel Flame went out</u>
<u>143</u>	<u>SL dryer</u>	<u>Start</u>	<u>started on oil, wood No 9 =</u>
<u>540</u>	<u>SL + CL dryer</u>	<u>stop</u>	<u>Power Bump</u>
<u>542</u>	<u>SL + CL dryer</u>	<u>start</u>	

Use Reverse side for additional space.

**APPENDIX F**  
**Equipment Calibration**  
**&**  
**CEMS Gas Certifications**

Probe Identification 401 Pitot Identification 401  
 Technical Specialist E.MOST  
 Date 4/26/96



$D_t$  0.374  
 $D_n$  0.500  
 $a$  0.785

$P_a$  0.567  
 $P_b$  0.567  
 $b$  1.067

$c$  5.073  
 $d$  4.502  
 $e$  0.792

OR

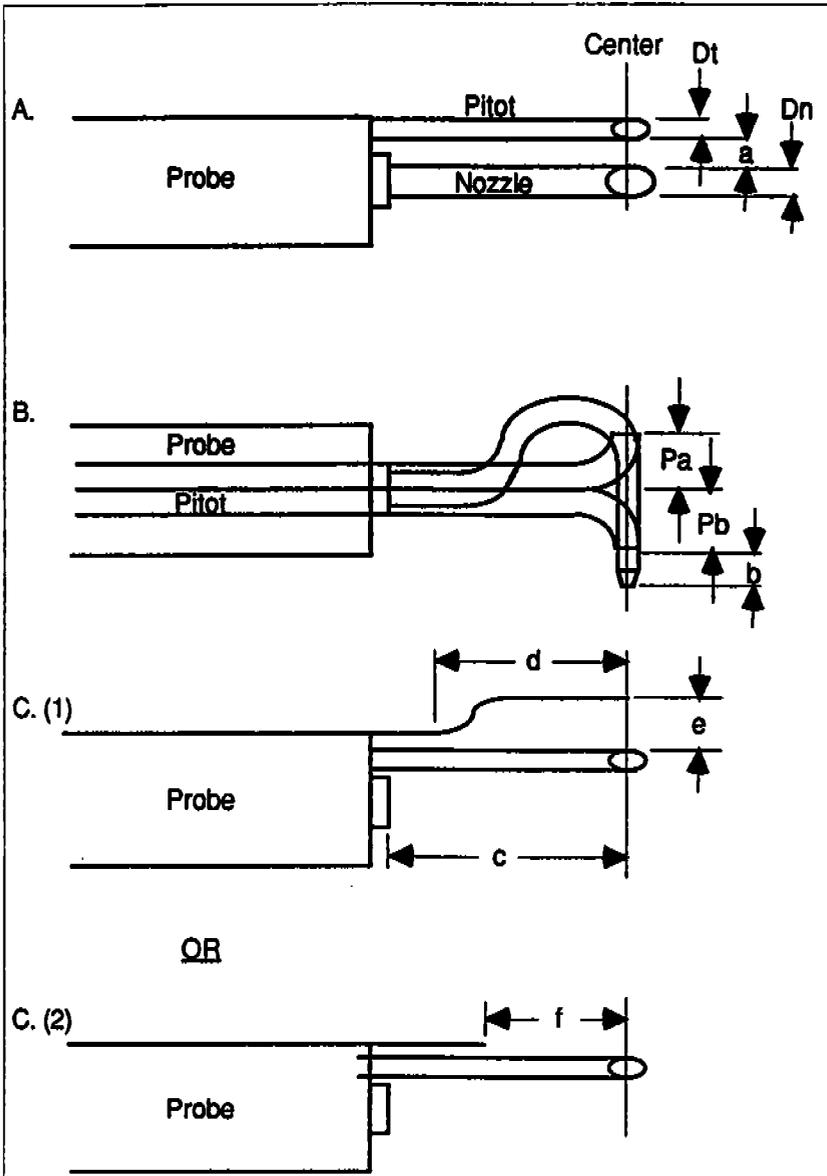
$c$  \_\_\_\_\_  
 $f$  \_\_\_\_\_

Specifications (EPA Method 2)

$D_t = 3/16''$  to  $3/8''$        $c \geq 3''$        $P_a = P_b$   
 $D_n = 1/2''$        $d \geq 3''$   
 $a \geq 3/4''$        $e \geq 3/4''$        $1.05 D_t \leq P \leq 1.50 D_t$   
 $b \geq 0$        $f \geq 2''$

If these specifications are met, proceed with Part 2, Pitot alignment.

Probe Identification 601 Pitot Identification 601  
 Technical Specialist EMOST  
 Date 4/26/96



Dt 0.374  
 Dn 0.622  
 a 0.753

Pa 0.517  
 Pb 0.517  
 b 0.923

c 5.312  
 d 3.360  
 e 0.782

OR

OR

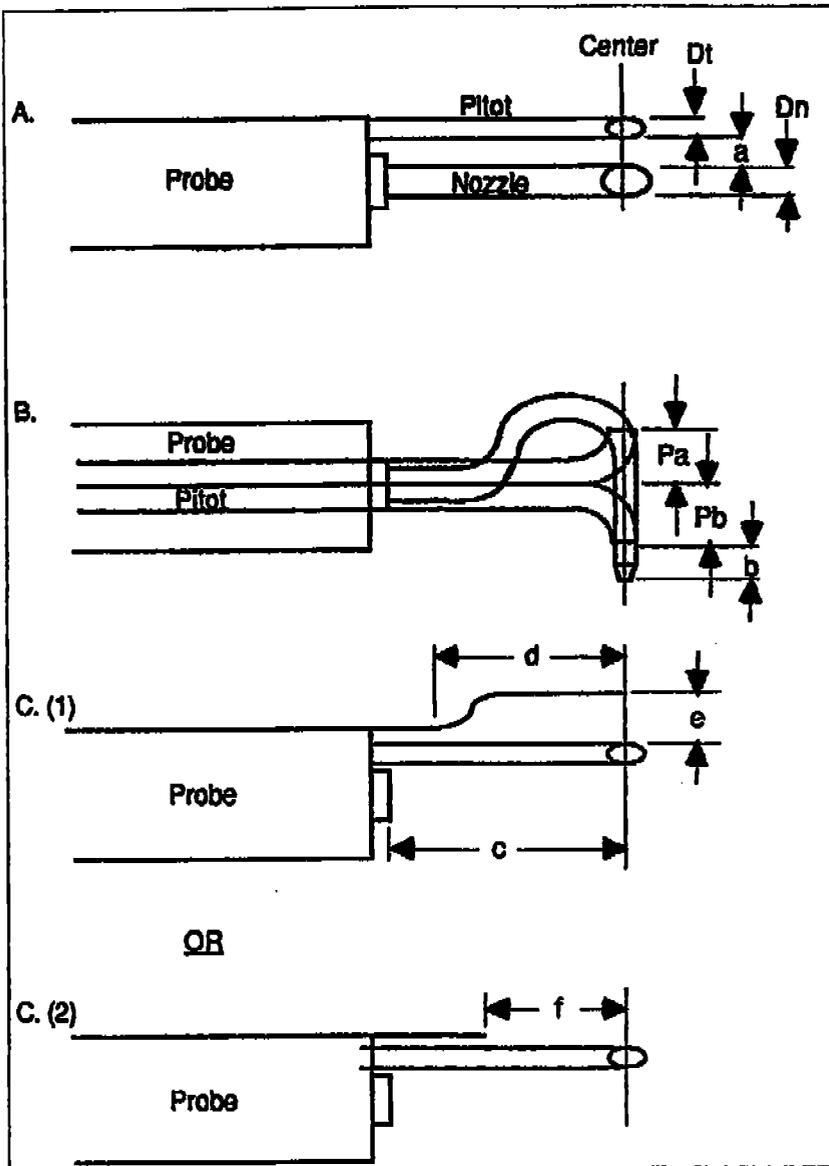
c \_\_\_\_\_  
 f \_\_\_\_\_

Specifications (EPA Method 2)

Dt = 3/16" to 3/8"	c ≥ 3"	Pa = Pb
Dn = 1/2"	d ≥ 3"	
a ≥ 3/4"	e ≥ 3/4"	1.05 Dt ≤ P ≤ 1.50 Dt
b ≥ 0	f ≥ 2"	

If these specifications are met, proceed with Part 2, Pitot alignment.

Probe Identification 902 Pitot Identification 902  
 Technical Specialist EMOST  
 Date 4/26/96



Dt 0.0378  
 Dn 0.625  
 a 0.778

Pa 0.515  
 Pb 0.515  
 b 0.778

c 5.897  
 d 4.375  
 e 1.059

OR

c \_\_\_\_\_  
 f \_\_\_\_\_

Specifications (EPA Method 2)

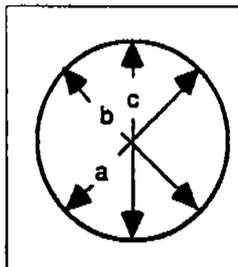
Dt = 3/16" to 3/8"      c ≥ 3"      Pa = Pb  
 Dn = 1/2"      d ≥ 3"  
 a ≥ 3/4"      e ≥ 3/4"      1.05 Dt ≤ P ≤ 1.50 Dt  
 b ≥ 0      f ≥ 2"

If these specifications are met, proceed with Part 2, Pitot alignment.

Nozzle Set Number #1 \_\_\_\_\_

Tech Specialist E. MOST

Date Calibrated 4/11/96



Nozzle Number	Diameter*	a	b	c	Average**
1-1	3/16	0.177	0.178	0.178	0.178
1-2	1/4	0.252	0.253	0.252	0.252
1-3	9/32	0.276	0.274	0.274	0.275
1-4	3/8	0.374	0.373	0.375	0.374
1-5	13/32	0.406	0.406	0.407	0.406
1-6	1/2	0.492	0.493	0.493	0.493
1-7	5/16	0.313	0.314	0.314	0.314
1-8	7/32	0.208	0.208	0.209	0.208

\*NOTE: Measure to the nearest 0.001".

\*\*NOTE: The three measurements must be within 0.004" of each other.

# CRITICAL ORIFICE METHOD 5 MODULE CALIBRATION

PUMP NUMBER: 3

MODULE NUMBER: 98

NAME: E. MOST

BAROMETRIC PRESSURE: 29.60

STANDARD METER DGM-115

PRE-CAL

POST-CAL FROM

MODULE			ORIFICE		MODULE METER							CALIBRATIONS				
PUMP VACUUM* (in. Hg)	ΔH SETTING (in. H2O)	TEMP. Tamb (°F)	NUMBER	K'	VOLUME Vml (cubic ft.)	VOLUME Vmf (cubic ft.)	VOLUME Vm (cubic ft.)	TEMP. Tmi (°F)	TEMP. Tmf (°F)	TEMP. Tm (°F)	TIME ∞ (min)	Vm (std)	Vcr (std)	Y	Variability	ΔH@
15	0.62	67	AC47	0.3146	501.27	503.39	2.12	66	66	66	5.00	2.11	2.03	0.96	-0.04	2.11
15	1.20	66	AC 55	0.4378	503.63	506.47	2.84	66	66	66	5.00	2.83	2.83	1.00	0.00	2.11
15	1.90	65	AC 63	0.5633	506.67	510.30	3.63	68	66	67	5.00	3.61	3.64	1.01	0.01	2.02
15	3.50	64	AC 73	0.7647	510.76	515.71	4.95	70	67	69	5.00	4.93	4.94	1.00	0.00	2.02
15	4.90	64	AC 81	0.9468	516.07	522.07	6.00	72	67	70	5.00	5.99	6.12	1.02	0.02	1.86
													1.00	0.00	2.03	

\*NOTE: Each orifice has a pre-calibrated critical vacuum of 14" Hg, set module vacuum at 1" to 2" above critical vacuum.

$$Vcr(std) = \frac{K Pbar^{\infty}}{\sqrt{Tamb}}$$

$$Vm(std) = 17.64 \frac{Vm (Pbar + \Delta H/13.6)}{(Tm + 460)}$$

$$Y = \frac{Vcr(std)}{Vm(std)}$$

$$\Delta H@ = 0.0319 \Delta H \frac{(Tm + 460)^{\infty/2}}{Pbar (YVm)^2}$$

Module Leak Check:  X  
 Pilot Leak Check:  X  
 Probe Heat Control:  X  
 Heater Box Control:  X  
 T.C. Readout calibrated with: Hot / Cold Bath  X  
 Constant Voltage Source

**\*\* CERTIFICATE OF ANALYSIS - EPA PROTOCOL MIXTURE \*\***

CUSTOMER: ABCO WELDING & INDUSTRIAL SUPPLY  
CYLINDER #: SX-37453  
CYLINDER PRESSURE: 2,000 psig  
LAST ANALYSIS DATE: 04-05-96  
EXPIRATION DATE: 04-05-99

REFERENCE #: 109-48682  
PROTOCOL: 1

**DO NOT USE THIS CYLINDER WHEN THE  
PRESSURE FALLS BELOW 150 psig**

Component: CARBON DIOXIDE

REPLICATE CONCENTRATIONS  
Date: 04-05-96

Mean Conc: 12.6 PCT

12.6 PCT  
12.6 PCT  
12.6 PCT

COMPONENT: OXYGEN

Date: 04-05-96

Date:

Mean Conc: 12.8 PCT

12.8 PCT  
12.8 PCT  
12.8 PCT

BALANCE GAS: NITROGEN

REFERENCE STANDARDS

SRM #: 1674B  
CYLINDER #: CLM-6492  
CONCENTRATION: 6.98 PCT

GMIS2659G  
SX-30352  
20.34 PCT

CERTIFICATION INSTRUMENTS

COMPONENT CARBON DIOXIDE  
MAKE/MODEL Horiba VIA 510  
SERIAL NUMBER 850802052  
MEASUREMENT PRINC. NDIR  
LAST CALIBRATION 03-19-96

OXYGEN  
Rosemount 755  
2002832  
Paramagnetic  
04-01-96

THIS CERTIFICATION WAS PERFORMED ACCORDING TO EPA TRACEABILITY PROTOCOL FOR  
ASSAY & CERTIFICATION OF GASEOUS CALIBRATION STANDARDS REVISED SEPT. 1993,  
USING PROCEDURE G1 AND/OR G2. THE TOTAL ANALYTICAL UNCERTAINTY OF THIS  
MIXTURE IS ESTIMATED TO BE ± OR - 1%.

ANALYST Thomas J. Purdon

DATE 4/10/96

\*\* CERTIFICATE OF ANALYSIS - EPA PROTOCOL MIXTURE \*\*

CUSTOMER: ABCO WELDING & INDUSTRIAL SUPPLY  
CYLINDER #: SX-37445  
CYLINDER PRESSURE: 2,000 psig  
LAST ANALYSIS DATE: 04-05-96  
EXPIRATION DATE: 04-05-99

REFERENCE #: 109-48682  
PROTOCOL: 1

DO NOT USE THIS CYLINDER WHEN THE  
PRESSURE FALLS BELOW 150 psig

Component: CARBON DIOXIDE  
Date: 04-05-96  
Mean Conc: 19.7 PCT  
19.7 PCT  
19.7 PCT  
19.6 PCT

COMPONENT: OXYGEN  
Date: 04-05-96  
Mean Conc: 22.6 PCT  
22.6 PCT  
22.6 PCT

BALANCE GAS: NITROGEN

REFERENCE STANDARDS  
SRM #: 1674B  
CYLINDER #: CLM-6492  
CONCENTRATION: 6.98 PCT  
GMIS2659G  
SX-30352  
20.34 PCT

CERTIFICATION INSTRUMENTS

COMPONENT	CARBON DIOXIDE	OXYGEN
MAKE/MODEL	Horiba VIA 510	Rosemount 755
SERIAL NUMBER	850802052	2002832
MEASUREMENT PRINC.	NDIR	Paramagnetic
LAST CALIBRATION	03-19-96	04-01-96

THIS CERTIFICATION WAS PERFORMED ACCORDING TO EPA TRACEABILITY PROTOCOL FOR  
ASSAY & CERTIFICATION OF GASEOUS CALIBRATION STANDARDS REVISED SEPT. 1993,  
USING PROCEDURE G1 AND/OR G2. THE TOTAL ANALYTICAL UNCERTAINTY OF THIS  
MIXTURE IS ESTIMATED TO BE + OR - 1%.

ANALYST Thomas J. Purdon DATE 4/15/96

# Scott Specialty Gases, Inc.

2330 HAMILTON BOULEVARD  
SOUTH PLAINFIELD NJ 07080  
Phone: 908-754-7700

Fax: 908-754-7303

## CERTIFICATE OF ANALYSIS

AIR POLLUTION CHARACTER  
EARL HEST  
AND CONTROL  
60 INDUSTRIAL PK RD WEST  
TOLLAND CT 06084

PROJECT #: 07-24580-004  
POM: CA1389  
ITEM #: 07022751 4AL  
DATE: 12/16/93

CYLINDER #: AL4008186

ANALYTICAL ACCURACY:  $\pm 2\%$

BLENDED TYPE: CERTIFIED MASTER GAS

COMPONENT  
METHANE  
NITROGEN

REQUESTED GAS  
CONC. MOLES  
275. PPM  
BAL

ANALYSIS  
(MOLES)  
283. PPM  
BAL

# CERTIFIED

ANALYST

JOHN O'SHEA

PLUMSTEADVILLE, PENNSYLVANIA / TROY, MICHIGAN / HOUSTON, TEXAS / DURHAM, NORTH CAROLINA  
SOUTH PLAINFIELD, NEW JERSEY / FREMONT, CALIFORNIA / WAKEFIELD, MASSACHUSETTS / LONGMONT, COLORADO  
BATON ROUGE, LOUISIANA

# Scott Specialty Gases, Inc.

RECEIVED JUL 2 - 1993

Shipped 2330 HAMILTON BOULEVARD  
From: SOUTH PLAINFIELD NJ 07080  
Phone: 908-754-7700

Fax: 908-754-7300

## CERTIFICATE OF ANALYSIS

ATP POLLUTION CHARACTER  
EARL MOST  
AND CONTROL  
60 INDUSTRIAL PK RD WEST  
TOLLAND CT 06084

PROJECT #: 07-21664-001  
PO#: 1194 EM  
ITEM #: 07022751 4AL  
DATE: 6/24/93

~~CYLINDER # 07-21664-001~~

ANALYTICAL ACCURACY:  $\pm$  2 %

BLEND TYPE : CERTIFIED MASTER GAS

COMPONENT	REQUESTED GAS	ANALYSIS
	CONC MOLES	(MOLES)
METHANE	500. PPM	<del>                    </del> PPM
NITROGEN	BAL	BAL

ANALYST:                     

JOHN O'SHEA

APPROVED BY:                     

ADELA SY

GREAT LAKES AIRGAS INC

\*\*\*\*\* CERTIFICATE OF ANALYSIS \*\*\*\*\*

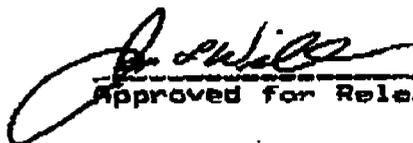
Customer: Connecticut Airgas

June 21 1995

Test Report GM 48195

PRIMARY STANDARD GRADE

CYLINDER NUMBER	REQUESTED COMPOSITION	REPORTED COMPOSITION
CC26728	900ppm Methane Balance Nitrogen	911ppm Methane Balance Nitrogen
CC97937	900ppm Methane Balance Nitrogen	901ppm Methane Balance Nitrogen

  
Approved for Release

**ANALYTICAL REPORT**

Report No: 33879  
 Date: 06-28-79  
 Purchase Order: 35-8227

at Connecticut Energy/Presto Div  
 441 Sackett Point Road  
 North Haven, CT 06473  
 203-288-9381

Order No: 33879

Item Ordered: 100 ppm Methane/Nitrogen Primary Standard

Order No:	Component	Specification	Concentration:
[REDACTED]	Methane Nitrogen	100 ppm Balance	[REDACTED] Balance

Name of Analyst: [REDACTED]  
 Organization: [REDACTED]

Comments: [REDACTED]



This report states only the results of the investigation made upon materials submitted to the analytical laboratory. Every effort has been made to determine objectively the information requested. However, in connection with the rendering of this report, CRYODYNE TECHNOLOGIES, INC. shall have no liability in excess of its established charge for the service. Any use of this report or the information contained herein shall be at the sole risk of the user.

NATIONAL SPECIALTY GASES  
630 UNITED DRIVE  
DURHAM, NC 27713  
(919)544-3772

CERTIFICATE OF ANALYSIS-EPA PROTOCOL MIXTURES

REFERENCE #: 89-37794  
CYL. PRESSURE: 2000PSIG  
ANALYSIS DATE: 2/1/95  
CUSTOMER: CONNECTICUT AIRGAS P.O.# 15645

METHOD: ANALYZED ACCORDING TO EPA TRACEABILITY PROTOCOL FOR ASSAY AND CERTIFICATION  
OF GASEOUS CALIBRATION STANDARDS-SEPTEMBER 1993:G-1

STANDARD: SRM #: 1659A  
CYL #: CLM3081  
CONC.: 9.65PPM  
INSTRUMENT: BECKMAN THC  
MODEL #: 400  
SERIAL #: 1003052  
LAST CAL.: 1/10/95

COMPONENT: CH4	COMPONENT:	COMPONENT:
REPLICATE CONC.	MEAN CONC:	MEAN CONC:
DATE: 2/1/95	REPLICATE CONC.	REPLICATE CONC.
DATE:	DATE:	DATE:
16.2PPM		
16.3PPM		
16.3PPM		

BALANCE GAS: N2

REPLICATE DATA

DATE: 2/1/95					
Z 0 R	348.0	C	584.2		
R 348.1 Z	0	C	588.0		
Z 0 C	588.2	R	348.2		

COMPONENT: CH4

DATE:					
Z	R				C
R	Z				C
Z	C				R

REPLICATE DATA

DATE:					
Z	R		C		
R	Z		C		
Z	C		R		

COMPONENT:

DATE:					
Z	R				C
R	Z				C
Z	C				R

REPLICATE DATA

DATE:					
Z	R		C		
R	Z		C		
Z	C		R		

COMPONENT:

DATE:					
Z	R				C
R	Z				C
Z	C				R

Z=ZERO C=CANDIDATE R=REFERENCE

ANALYST: *Gracy A. Savoy*

APPROVED BY: *John D. ...*

THIS REPORT STATED ACCURATELY THE RESULTS OF THE INVESTIGATION MADE UPON THE MATERIAL SUBMITTED TO THE ANALYTICAL LABORATORY. EVERY EFFORT HAS BEEN MADE TO DETERMINE OBJECTIVELY, THE INFORMATION REQUESTED; HOWEVER, IN CONNECTION WITH ITS RENDERING OF THIS REPORT, NATIONAL SPECIALTY GASES SHALL HAVE NO LIABILITY IN EXCESS OF ITS ESTABLISHED CHARGE FOR THE SERVICE.

GREAT LAKES AIRGAS INC

\*\*\*\*\* CERTIFICATE OF ANALYSIS \*\*\*\*\*

Customer: Connecticut Airgas

May 16 1995

Test Report GM 35895

PRIMARY MIXTURE

CYLINDER NUMBER	REQUESTED COMPOSITION	REPORTED COMPOSITION
[REDACTED]	50ppm Methane Balance Nitrogen	[REDACTED] 50ppm Methane Balance Nitrogen
[REDACTED]	50ppm Methane Balance Nitrogen	[REDACTED] 50ppm Methane Balance Nitrogen

Post-It® Fax Note 7571

Date	6-9	# of pages	1
From	RAY		
To	PETER		
Co. Dept	APCC		
Phone #			
Fax #	871-8625		

INV. 72805

Ed Johnson  
Approved for Release

GREAT LAKES AIRGAS INC

\*\*\*\*\* CERTIFICATE OF ANALYSIS \*\*\*\*\*

Customer: Connecticut Airgas

May 13 1995

Test Report GM 35995

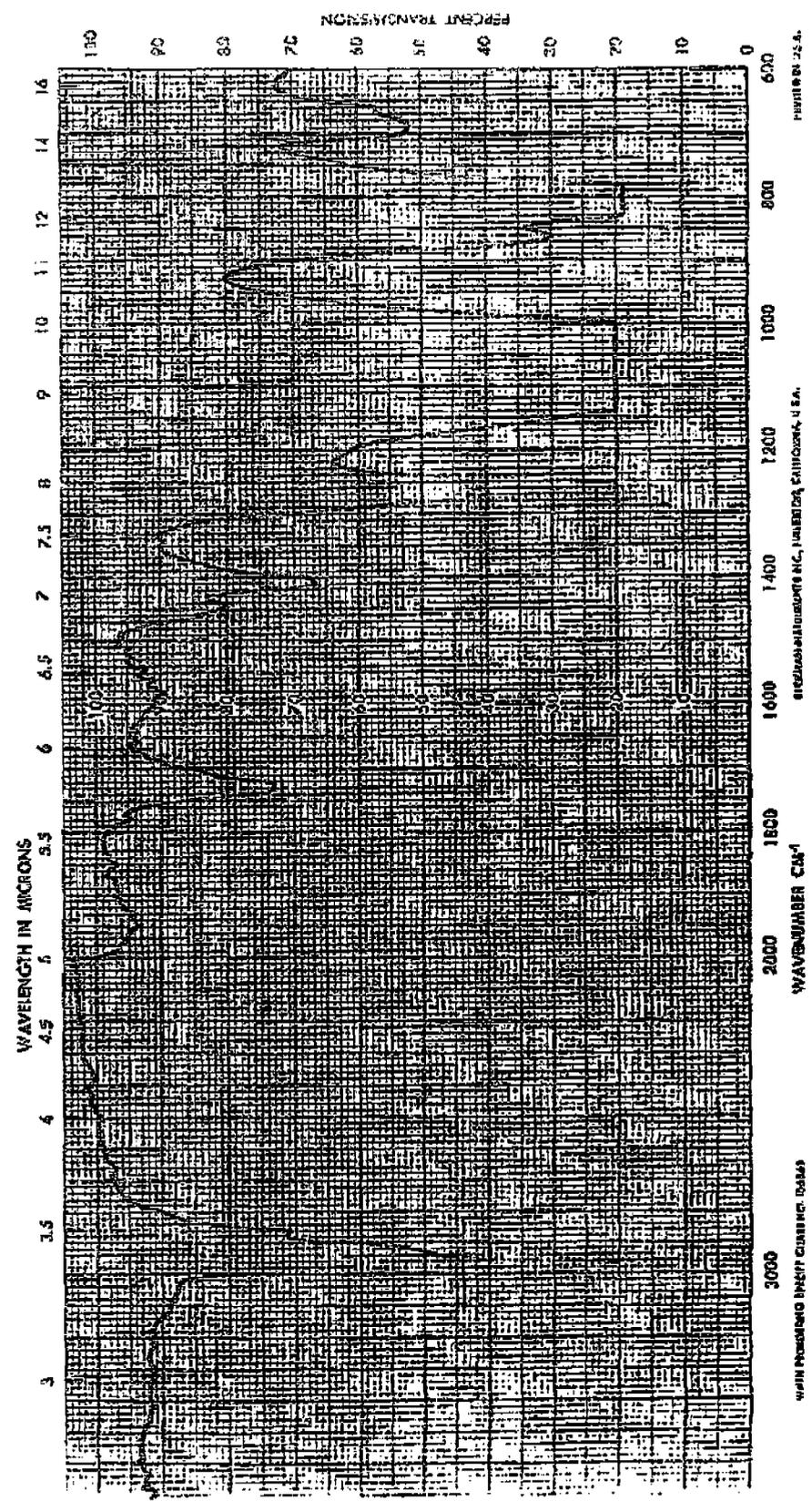
PRIMARY MIXTURE

CYLINDER NUMBER	REQUESTED COMPOSITION	REPORTED COMPOSITION
[REDACTED]	35ppm Methane Balance Nitrogen	[REDACTED] Methane Balance Nitrogen
[REDACTED]	35ppm Methane Balance Nitrogen	[REDACTED] Methane Balance Nitrogen

*Ed Johnson*  
Approved for Release

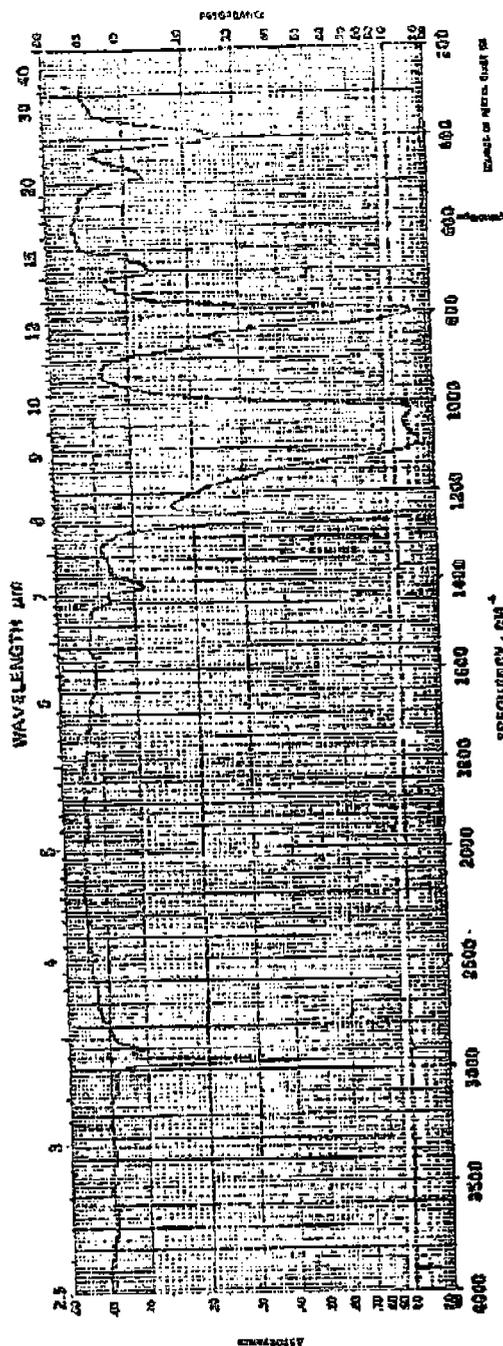
**APPENDIX G**  
**Laboratory Data**

*Thin film IR scan*  
*Test 4 / Run 1 organic*



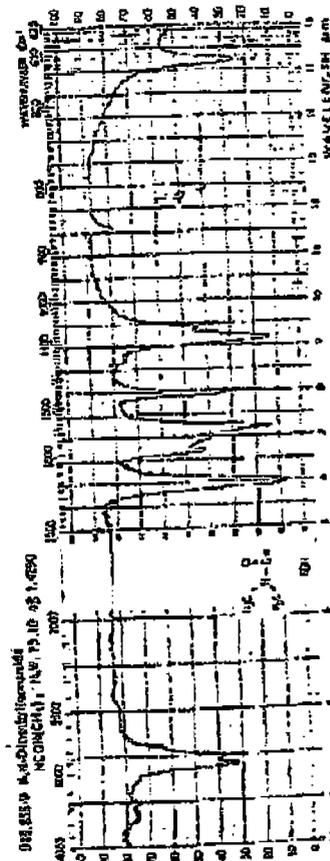
Source: Dow Corning Corp.  
Capillary Cell

SILICONE LUBRICANT



IR SPECTRUM IDENTIFICATION  
LAB NUMBER: 10K, D.L.S.

IR Scan  
Starts @ 600



Vertical text on the right edge of the page, possibly a document ID or page number.



INTERPOLL LABORATORIES, INC.  
4500 BALL ROAD N.E.  
CIRCLE PINES, MINNESOTA 55014-1819  
TEL: 612/786-6020  
FAX: 612/786-7854

August 30, 1996

Sue Somers  
Louisiana-Pacific Corporation  
Northern Division  
Rt. 8, Box 8263  
Hayward, Wisconsin 54843

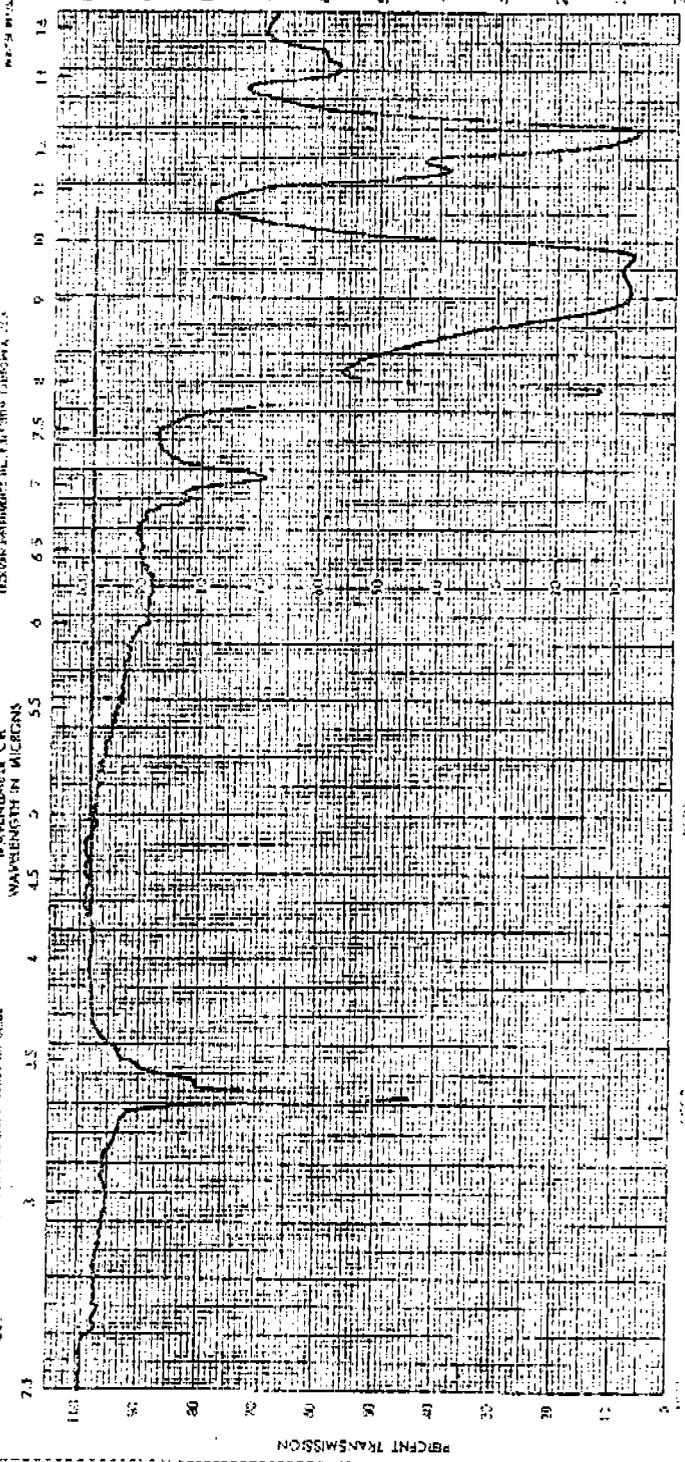
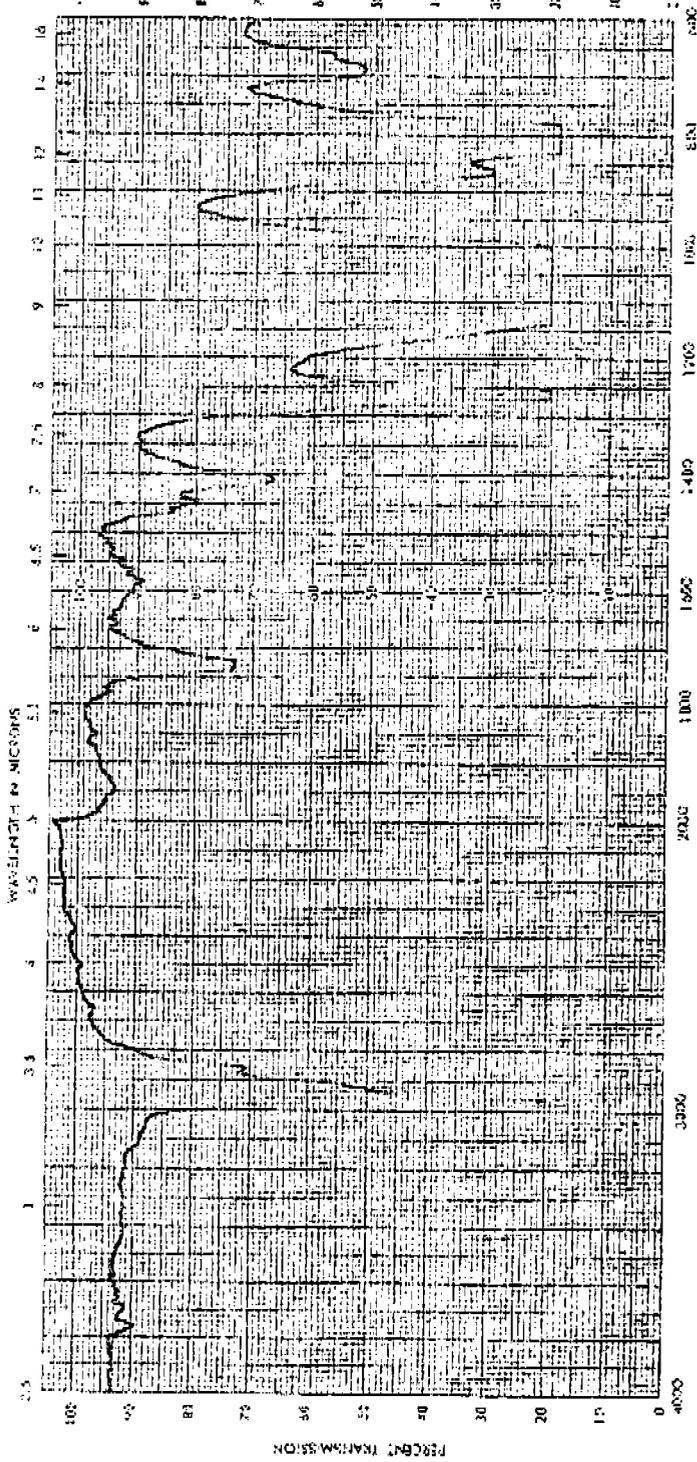
Dear Sue:

Interpoll Laboratories, Inc. received six (6) samples representing the organic and inorganic EPA Method 202 samples from Test 4, Runs 1-3. These samples were collected from the Dryer RTO Stack at the Louisiana-Pacific facility located in Houlton, Maine. The reason these samples were submitted to Interpoll Labs was the high organic fraction determined for Run 1 which appeared to be an outlier. The organic fraction of Run 1 was therefore resolubilized in methylene chloride and a thin film applied to a sodium chloride plate for infrared analysis. This technique was chosen as it is a nondestructive technique which would provide additional information as to the composition of the material. The instrument used in this work is a Beckman Microlab 600 Computing IR Spectrophotometer. The result of this IR scan is provided on the attachment. A tentative identification of this material was silicone grease, a common glass joint sealant used by most stack testing firms, however, use of this sealant is not recommended when performing EPA Method 202 as the methylene chloride does extract this compound from glass surfaces. A sample of Dow Corning silicone grease was therefore also run to provide a reference spectra, the result of that IR scan is shown below the sample run. A comparison of these two spectra indicate that the Test 4 Run 1 organic fraction does contain silicone grease. Note that this technique is not quantitative, therefore the exact amount of silicone grease cannot be determined, however, the "purity" of the spectra indicate that the sample contained a substantial quantity of silicone grease. Note that the other two organic fractions (Runs 2 & 3) were analyzed and found to contain silicone grease also.

Should you have any questions please do not hesitate to call me.

Sincerely,  
INTERPOLL LABORATORIES, INC.

Daniel Despen,  
Manager  
Stationary Source Testing Department



SPECTRUM NO. \_\_\_\_\_  
 DATE 8/30/98  
 SAMPLE # 8755-102  
 SOURCE \_\_\_\_\_  
 STRUCTURE \_\_\_\_\_  
 PATH \_\_\_\_\_ mm  
 SOLVENT \_\_\_\_\_  
 CONCENTRATION \_\_\_\_\_  
 PHASE \_\_\_\_\_  
 COMMENTS \_\_\_\_\_  
 ANALYST LAW



INFRARED  
 SPECTROPHOTOMETER

SPECTRUM NO. \_\_\_\_\_  
 DATE 8/30/98  
 SAMPLE # 8755-102  
 SOURCE \_\_\_\_\_  
 STRUCTURE \_\_\_\_\_  
 PATH \_\_\_\_\_ mm  
 SOLVENT \_\_\_\_\_  
 CONCENTRATION \_\_\_\_\_  
 PHASE \_\_\_\_\_  
 COMMENTS \_\_\_\_\_  
 ANALYST LAW



INFRARED  
 SPECTROPHOTOMETER