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**RESULTS OF THE JUNE 7 - 10, 1994
AIR EMISSION COMPLIANCE TESTS
AT THE LOUISIANA PACIFIC OSB
PLANT IN HAYWARD, WISCONSIN**

Submitted to:

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SP/slp

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ABBREVIATIONS

ACFM	actual cubic feet per minute
cc (ml)	cubic centimeter (milliliter)
DSCFM	dry standard cubic foot of dry gas per minute
DSML	dry standard milliliter
DEG-F (°F)	degrees Fahrenheit
DIA.	diameter
FP	finished product for plant
FT/SEC	feet per second
g	gram
GPM	gallons per minute
GR/ACF	grains per actual cubic foot
GR/DSCF	grains per dry standard cubic foot
g/dscm	grams per dry standard cubic meter
HP	horsepower
HRS	hours
IN.	inches
IN.HG.	inches of mercury
IN.WC.	inches of water
LB	pound
LB/DSCF	pounds per dry standard cubic foot
LB/HR	pounds per hour
LB/10 ⁶ BTU	pounds per million British Thermal Units heat input
LB/MMBTU	pounds per million British Thermal Units heat input
LTPD	long tons per day
MW	megawatt
mg/Nm ³	milligrams per dry standard cubic meter
ug/Nm ³	micrograms per dry standard cubic meter
microns (um)	micrometer
MIN.	minutes
ng	nanograms
ohm-cm	ohm-centimeter
PM	particulate matter
PPH	pounds per hour
PPM	parts per million
ppmC	parts per million carbon
ppm,d	parts per million, dry
ppm,w	parts per million, wet
ppt	parts per trillion
PSI	pounds per square inch
SQ.FT.	square feet
TPD	tons per day
ug	micrograms
v/v	percent by volume
w/w	percent by weight
<	≤ (when following a number)

Standard conditions are defined as 68°F (20°C) and 29.92 IN. of mercury pressure.

1 INTRODUCTION

During the Period June 7 - 10, 1994 Interpoll Laboratories personnel conducted air emission compliance tests on the following sources at the Louisiana Pacific Corporation (LP) OSB Plant located in Hayward, Wisconsin.

Source	Parameters
Line 1 Press RTO Inlet	PM, THC's ^{VOC}
Line 1 Press RTO Outlet Stack	PM, NO _x , VE, CO, CH ₂ O, MDI, THC's
Line 1 Konus Stack	PM, NO _x , VE, CO, CH ₂ O, POM's, Phenol, Benzene
Line 2 Press RTO Inlet	PM, THC's
Line 2 Press RTO Outlet Stack	PM, NO _x , VE, CO, CH ₂ O, MDI, THC's
Line 2 Konus Stack	PM, NO _x , VE, CO, CH ₂ O, POM's, Phenol, Benzene

On-site testing was performed by Duane Van Hoever, Scott Bainville, Ed Trowbrige, Mark Kaehler, Ed Juers, Dave Vaaler, Ken Rosenthal, Dennis Marso, and Ken Nuessmeier. Coordination between testing activities and plant operation was provided by Sue Somers of LP. The test was witnessed by Jim Ross, Brad Pyle, and Judy Hayducsko of the Wisconsin Department of Natural Resources and Basim Dihu of the Environmental Protection Agency.

The thermal oil heaters tested were manufactured by Konus and are equipped with underfed stokers (pile burners). The oil heaters are fired with bark and wet fines wood waste. The net heat output capacity is 13 10⁶ BTU/HR for the No. 1 and 2 Konus heaters (each unit). Particulate emissions from each oil heater are controlled by Konus multiclones. Cleaned flue gas from the Nos. 1 and 2 Konus heaters exhaust to the atmosphere via a common stack as does the flue gas from the Nos. 3 and 4 Konus heaters. From the multiclones, the exhaust from each pair of Konuses (1 and 2, 3 and 4) is then controlled by an Electrified Filter Bed Manufactured by EFB.

The press vents tested are the exhaust from hoods positioned over the board press and unloader. Particulate emissions are controlled with a Regenerative Thermal Oxidizer (RTO) manufactured by Huntington.

Particulate evaluations were performed in accordance with EPA Methods 2-5, CFR Title 40, Part 60, Appendix A (revised July 1, 1993). A preliminary determination of the gas linear velocity profile was made at each test location before the first particulate determination to allow selection of the appropriate nozzle diameter for isokinetic sample withdrawal. An Interpoll Labs sampling train which meets or exceeds specifications in the above-cited reference was used to isokinetically extract particulate samples by means of a heated glass-lined probe. Wet catch samples were collected in the back half of the Method 5 sampling train and analyzed in accordance with Wisconsin DNR protocol.

Carbon monoxide determinations were performed in accordance with Method 10. A slip stream of sample gas was withdrawn from the exhaust gas stream using a heated stainless steel probe equipped with a filter to remove interfering particulate material. The particulate-free gas was transported to the analyzers by means of a heat-traced probe and filter assembly. After passing through the filter, the gas passed through a chilled condenser-type moisture removal system. The particulate-free dry gas was then transported to the analyzers with the excess exhausted to the atmosphere through a calibrated orifice which was used to ensure that the flow from the stack exceeds the requirements of the analyzers. A three-way valve on the probe was used to introduce standard gas for the "system bias check".

The analog response of the carbon monoxide analyzer was recorded with a strip chart recorder. The analyzer was calibrated with Scott Specialty, National Specialty, and Linde Gases (EPA Protocol 1) and Certified Master standard gases. The instrument was calibrated before and after each run as per EPA Method 10. The sample probe was moved through a three-point traverse (1/6, 3/6, 5/6 of the stack diameter) to measure carbon monoxide concentrations.

Formaldehyde samples were collected using EPA Method 0011 (SW 846 3rd Ed.). The samples were collected isokinetically using a Method 5 sampling train with an aqueous acidic 2,4-dinitrophenylhydrazine absorbing solution and analyzed by high performance liquid chromatography.

Total gaseous hydrocarbon concentrations were determined instrumentally using a Ratfisch Model RS55 heated flame ionization detector (HFID) calibrated against propane in

air standards. The THC concentration was continuously monitored by extracting a slipstream of exhaust gas by means of a heated probe and filter holder. A heat-traced teflon line was used to transport the sample gas from the filter holder outlet to the analyzer inlet.

Phenol concentrations were determined from the Press Vent using a Method 5 sampling train with neutral buffered absorbing reagent followed by extraction with methylene chloride and direct analysis by GC/MS with no concentration (EPA Method 8270). The samples were field spiked with 5.33 mg of phenol d5.

Polyaromatic hydrocarbons sampling was conducted using the EPA Modified Method 5 sampling procedure as per EPA Method 010 SW 846. The four-part sample and field blank were extracted, concentrated to 1000 ul and cleaned up as required (column chromatography as per Interpoll Labs Method II-8904-2 or GPC) prior to final concentration and analysis. The samples were then further concentrated to 100 ul and analyzed in accordance with EPA Method 8270 by HRGC/LRMS using electron impact (EI) with total ion monitoring (TIM). Quantification was performed using the six standard M-8270 internal standards. Each XAD-2 resin cartridge was field spiked with 20 ug of d₁₀-fluoroanthene in order to document overall collection and analytical efficiency and recovery. Analytical accuracy and recovery for extraction and cleanup was documented using the six m-8270-recommended surrogate standards.

MDI concentrations were determined in accordance with the 1,2-PP Method as developed by Radian Corporation under contract to USEPA. This method employs collection of MDI with 1,2-PP in toluene reagent, with analysis by HPLC.

Benzene samples were collected in accordance with EPA Method 18 Section 7.4. Charcoal tubes were used for sampling with analysis by GC/FID.

Integrated flue gas samples were extracted simultaneously with each of the above-referenced sampling trains at the dryer test site using a specially designed gas sampling system. Integrated flue gas samples were collected in 44-liter Tedlar bags housed in a protective aluminum container. After sampling was complete, the bags were sealed and returned to the laboratory for Orsat analysis. Prior to sampling, the Tedlar bags are leak checked at 15 IN.HG. vacuum with an in-line rotameter. Bags with any detectable inleakage

are discarded. The integrated flue gas samples collected were analyzed for carbon monoxide in accordance with EPA Method 10 (NDIR).

Testing on the Line 1 Press RTO Stack was conducted from two test ports oriented at 90 degrees on the stack. These test ports are located 5.7 stack diameters downstream of the nearest flow disturbance and 4.5 stack diameters upstream of the stack exit. A 20-point traverse was used to collect the particulate, formaldehyde, and MDI samples. Each traverse point was sampled 3 minutes for a total of 60 minutes per run.

Testing on the Line 1 Press RTO Inlet was conducted from two test ports oriented at 90 degrees. A 24-point traverse was used to collect the particulate samples. Each traverse point was sampled 2.5 minutes for a total of 60 minutes per run.

Testing on the Line 2 Press RTO Stack was conducted from two test ports oriented at 90 degrees on the stack. These test ports are located 5.7 stack diameters downstream of the nearest flow disturbance and 4.5 stack diameters upstream of the stack exit. A 20-point traverse was used to collect the particulate, formaldehyde, and MDI samples. Each traverse point was sampled 3 minutes for a total of 60 minutes per run.

Testing on the Line 2 Press RTO Inlet was conducted from two test ports oriented at 90 degrees. A 12-point traverse was used to collect the particulate samples. Each traverse point was sampled 5 minutes for a total of 60 minutes per run.

Testing on the Line 1 Konus Stack was conducted from two test ports oriented at 90 degrees on the stack. These test ports are located 5.2 diameters downstream and 2.8 diameters upstream of the nearest flow disturbances. A 20-point traverse was used to collect the particulate and formaldehyde samples. Each point was sampled for 3 minutes for a total sampling time of 60 minutes per run. A 24-point traverse was used to collect representative PAH samples. Each point was sampled for 2.5 minutes for a total sampling time of 60 minutes per run. A 3-point traverse was used to collect representative benzene samples.

Testing on the Line 2 Konus Stack was conducted from two test ports oriented at 90 degrees on the stack. These test ports are located 3.5 diameters downstream and 8 diameters upstream of the nearest flow disturbances. A 24-point traverse was used to collect the

particulate, formaldehyde, and PAH samples. Each point was sampled for 2.5 minutes for a total sampling time of 60 minutes per run. A 3-point traverse was used to collect representative benzene samples. Visible emissions determinations were performed on each stack by Ed Juers and Dave Vaaler, both of which are EPA-certified observers.

The important results of the test are summarized in Section 2. Detailed results are presented in Section 3. Field data and all other supporting information are presented in the appendices.

2 SUMMARY AND DISCUSSION

The results of the air emission compliance tests are summarized in Tables 1 - 16. An overview of the results is presented in the Table below:

PARAMETER MEASURED

Line 1 RTO Press Inlet

Particulate	
..... (GR/DSCF)	0.0124
..... (LB/HR)	6.5
Total Hydrocarbons	
..... (ppmC,w)	64
..... (LB/HR)	7.5

Line 1 Press RTO Stack

PM Removal Efficiency	(%)	17.6
THC Removal Efficiency	(%)	95.0
Particulate		
..... (GR/DSCF)		0.0094
..... (LB/HR)		5.4
Opacity	(%)	0
Oxides of Nitrogen		
..... (ppm,d)		19
..... (LB/HR)		9
Carbon Monoxide		
..... (ppm,d)		12
..... (LB/HR)		3.5
Total Hydrocarbons		
..... (ppmC,w)		3
..... (LB/HR)		0.36
Formaldehyde		
..... (ppm,d)		0.19
..... (LB/HR)		0.061
MDI		
..... (ppm)		≤ 0.0004
..... (LB/HR)		≤ 0.001

PARAMETER**MEASURED****Line 2 RTO Inlet****Particulate**

..... (GR/DSCF)	0.136
..... (LB/HR)	99.8

Total Hydrocarbons

..... (ppmC,w)	65
..... (LB/HR)	10.5

Line 2 Press RTO Stack

<i>PM Removal Efficiency</i> (%)	91.1
--	------

<i>THC Removal Efficiency</i> (%)	97.6
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Particulate

..... (GR/DSCF)	0.0129
..... (LB/HR)	8.9

Opacity (%)	0
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Oxides of Nitrogen

..... (ppm,d)	11
..... (LB/HR)	6.7

Carbon Monoxide

..... (ppm,d)	15
..... (LB/HR)	3.9

Total Hydrocarbons

..... (ppmC,w)	1.6
..... (LB/HR)	0.25

Formaldehyde

..... (ppm,d)	0.22
..... (LB/HR)	0.082

MDI

..... (ppm)	≤ 0.0005
..... (LB/HR)	≤ 0.002

<u>PARAMETER</u>	<u>MEASURED</u>
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Line 1 Konus Stack

Particulate

..... (GR/DSCF)	0.0278
..... (LB/10 ⁶ BTU)	0.125
..... (LB/HR)	2.61

Oxides of Nitrogen

..... (ppm,d)	76
..... (LB/10 ⁶ BTU)	0.291
..... (LB/HR)	5.95

Opacity	0
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Carbon Monoxide

..... (ppm,d)	115
..... (LB/10 ⁶ BTU)	0.269
..... (LB/HR)	5.41

Formaldehyde

..... (ppm,d)	0.05
..... (LB/HR)	0.0028

Phenol

..... (ppb)	< 175
..... (LB/HR)	< 28

Benzene

..... (ppm,d)	< 0.0114
..... (LB/HR)	< 0.0015

PARAMETER**MEASURED****Line 2 Konus Stack****Particulate**

..... (GR/DSCF)	0.0185
..... (LB/10 ⁶ BTU)	0.114
..... (LB/HR)	2.58

Oxides of Nitrogen

..... (ppm,d)	63
..... (LB/10 ⁶ BTU)	0.323
..... (LB/HR)	7.24

Opacity	(%)	0.96
---------------	-----	------

Carbon Monoxide

..... (ppm,d)	67
..... (LB/10 ⁶ BTU)	0.213
..... (LB/HR)	4.78

Formaldehyde

..... (ppm,d)	0.05
..... (LB/HR)	0.0044

Phenol

..... (ppb)	< 176
..... (LB/HR)	< 43

Benzene

..... (ppm,d)	< 0.011
..... (LB/HR)	< 0.0024

No difficulties were encountered in the field by Interpoll Labs or in the laboratory evaluation of the samples which were conducted by Interpoll Labs. On the basis of these facts and a complete review of the data and results, it is our opinion that the results reported herein are accurate and closely reflect the actual values which existed at the time the test was performed.

Table 1a Summary of the Results of the June 10, 1994 Particulate Emission Compliance Test on the Line 1 Press RTO Outlet Stack at the Louisiana Pacific Corporation Plant Located in Hayward, Wisconsin.

ITEM	Run 1	Run 2	Run 3
Date of test	06-10-94	06-10-94	06-10-94
Time runs were done (HRS)	935/1036	1100/1201	1220/1321
Volumetric flow actual (ACFM) standard (DSCFM)	98861 68420	96534 65961	97230 66157
Gas temperature (DEG-F)	259	264	268
Moisture content (%V/V)	2.45	3.06	2.93
Gas composition (%V/V, dry) carbon dioxide oxygen nitrogen	0.40 20.50 79.10	0.40 20.50 79.10	0.40 20.50 79.10
Isokinetic variation (%)	99.3	99.0	99.8
Particulate concentration actual (GR/ACF) standard (GR/DSCF)	.00737 .0107	.00657 .00962	.00530 .00779
Part. emission rate (LB/HR)	6.25	5.44	4.42

Note: Dry + Organic/Inorganic Wet Catch

Table 1b Summary of the Results of the June 10, 1994 Particulate Emission Compliance Test on the Line 1 Press RTO Outlet Stack at the Louisiana Pacific Corporation Plant Located in Hayward, Wisconsin.

ITEM	Run 1	Run 2	Run 3
Date of test	06-10-94	06-10-94	06-10-94
Time runs were done (HRS)	935/1036	1100/1201	1220/1321
Volumetric flow actual (ACFM) standard (DSCFM)	98861 .68420	96534 65961	97230 66157
Gas temperature (DEG-F)	259	264	268
Molsture content (%V/V)	2.45	3.06	2.93
Gas composition (%V/V, dry) carbon dioxide oxygen nitrogen	0.40 20.50 79.10	0.40 20.50 79.10	0.40 20.50 79.10
Isokinetic variation (%)	99.3	99.0	99.8
Particulate concentration actual (GR/ACF) standard (GR/DSCF)	.00412 .00596	.00222 .00324	.00218 .00321
Part. emission rate (LB/HR)	3.50	1.83	1.82

Note: Dry Catch Only

Table 2a Summary of the Results of the June 8, 1994 Particulate Emission Compliance Test on the Line 1 Konus Stack at the Louisiana Pacific Corporation Plant Located in Hayward, Wisconsin.

ITEM	Run 1	Run 2	Run 3
Date of test	06-08-94	06-08-94	06-08-94
Time runs were done (HRS)	1538/1640	1708/1811	1835/1938
Volumetric flow actual standard (ACFM) (DSCFM)	17975 10771	18652 11266	18575 10936
Gas temperature (DEG-F)	310	314	314
Moisture content (%V/V)	9.70	8.55	10.88
Gas composition (%V/V, dry) carbon dioxide oxygen nitrogen	6.00 14.50 79.50	5.00 15.50 79.50	7.00 13.50 79.50
Isokinetic variation (%)	102.1	99.3	102.4
Particulate concentration actual standard (GR/ACF) (GR/DSCF)	.0223 .0373	.0126 .0209	.0149 .0253
Part. emission rate (LB/HR)	3.44	2.02	2.37

Note: Dry + Organic/Inorganic Wet Catch

Table 2b Summary of the Results of the June 8, 1994 Particulate Emission Compliance Test on the Line 1 Konus Stack at the Louisiana Pacific Corporation Plant Located in Hayward, Wisconsin.

ITEM	Run 1	Run 2	Run 3
Date of test	06-08-94	06-08-94	06-08-94
Time runs were done (HRS)	1538/1640	1708/1811	1835/1938
Volumetric flow actual (ACFM) standard (DSCFM)	17975 10771	18652 11266	18575 10936
Gas temperature (DEG-F)	310	314	314
Moisture content (%V/V)	9.70	8.55	10.88
Gas composition (%V/V.dry) carbon dioxide oxygen nitrogen	6.00 14.50 79.50	5.00 15.50 79.50	7.00 13.50 79.50
Isokinetic variation (%)	102.1	99.3	102.4
particulate concentration actual (GR/ACF) standard (GR/DSCF)	.0195 .0326	.00757 .0125	.0122 .0208
Part. emission rate (LB/HR)	3.01	1.21	1.95

Note: Dry Catch Only

Table 3a Summary of the Results of the June 10, 1994 Particulate Emission Compliance Test on the Line 1 Press RTO Inlet at the Louisiana Pacific Corporation Plant Located in Hayward, Wisconsin.

ITEM	Run 1	Run 2	Run 3
Date of test	06-10-94	06-10-94	06-10-94
Time runs were done (HRS)	935/1037	1100/1205	1220/1322
Volumetric flow actual (ACFM) standard (DSCFM)	71543 61212	72779 61735	72499 61233
Gas temperature (DEG-F)	121	123	126
Moisture content (%V/V)	1.92	2.46	2.30
Gas composition (%V/V, dry) carbon dioxide oxygen nitrogen	0.03 20.90 79.07	0.03 20.90 79.07	0.03 20.90 79.07
Isokinetic variation (%)	99.8	100.6	100.1
Particulate concentration actual (GR/ACF) standard (GR/DSCF)	.0124 .0145	.00827 .00976	.0109 .0130
Part. emission rate (LB/HR)	7.59	5.16	6.81

72,274

123

dry
0.024

6.52

Note: Dry + Organic/Inorganic Wet Catch

Table 3b Summary of the Results of the June 10, 1994 Particulate Emission Compliance Test on the Line 1 Press RTO Inlet at the Louisiana Pacific Corporation Plant Located in Hayward, Wisconsin.

ITEM	Run 1	Run 2	Run 3
Date of test	06-10-94	06-10-94	06-10-94
Time runs were done (HRS)	935/1037	1100/1205	1220/1322
Volumetric flow actual standard (ACFM) (DSCFM)	71543 61212	72779 61735	72499 61233
Gas temperature (DEG-F)	121	123	126
Moisture content (%V/V)	1.92	2.46	2.30
Gas composition (%V/V, dry) carbon dioxide oxygen nitrogen	0.03 20.90 79.07	0.03 20.90 79.07	0.03 20.90 79.07
Isokinetic variation (%)	99.8	100.6	100.1
Particulate concentration actual standard (GR/ACF) (GR/DSCF)	.00745 .00871	.00390 .00460	.00699 .00828
Part. emission rate (LB/HR)	4.57	2.43	4.34

Note: Dry Catch Only

Table 4a Summary of the Results of the June 9, 1994 Particulate Emission Compliance Test on the Line 2 Press RTO Outlet Stack at the Louisiana Pacific Corporation Plant Located in Hayward, Wisconsin.

ITEM	Run 1	Run 2	Run 3
Date of test	06-09-94	06-09-94	06-09-94
Time runs were done (HRS)	1240/1342	1425/1527	1605/1719
Volumetric flow actual standard	117314 81742	116983 80986	114900 79766
			116399 80831
Gas temperature (DEG-F)	253	256	258
Moisture content (%V/V)	2.35	2.55	2.05
Gas composition (%V/V, dry)			
carbon dioxide	0.40	0.40	0.40
oxygen	20.60	20.60	20.55
nitrogen	79.00	79.00	79.05
Isokinetic variation (%)	99.6	99.9	99.6
Particulate concentration actual (GR/ACF)	.0145	.00495	.00738
standard (GR/DSCF)	.0208	.00715	.0106
Part. emission rate (LB/HR)	14.57	4.96	7.27

Note: Dry + Organic/Inorganic Wet Catch

Table 4b Summary of the Results of the June 9, 1994 Particulate Emission Compliance Test on the Line 2 Press RTO Outlet Stack at the Louisiana Pacific Corporation plant Located in Hayward, Wisconsin.

ITEM	Run 1	Run 2	Run 3
Date of test	06-09-94	06-09-94	06-09-94
Time runs were done (HRS)	1240/1342	1425/1527	1605/1719
Volumetric flow actual (ACFM) standard (DSCFM)	117314 81742	116983 80986	114900 79766
Gas temperature (DEG-F)	253	256	258
Moisture content (%V/V)	2.35	2.55	2.05
Gas composition (%V/V, dry) carbon dioxide oxygen nitrogen	0.40 20.60 79.00	0.40 20.60 79.00	0.40 20.55 79.05
Isokinetic variation (%)	99.6	99.9	99.6
Particulate concentration actual (GR/ACF) standard (GR/DSCF)	.0109 .0157	.00256 .00370	.00479 .00691
Part. emission rate (LB/HR)	10.97	2.57	4.72

Note: Dry Catch Only

Table 5a Summary of the Results of the June 8, 1994 Particulate Emission Compliance Test on the Line 2 Konus Stack at the Louisiana Pacific Corporation Plant Located in Hayward, Wisconsin.

ITEM	Run 1	Run 2	Run 3
Date of test	06-08-94	06-08-94	06-08-94
Time runs were done (HRS)	757/ 858	920/1021	1114/1215
Volumetric flow actual standard (ACFM) (DSCFM)	27063 16583	26771 16372	26291 15772
Gas temperature (DEG-F)	319	317	325
Moisture content (%V/V)	6.60	6.99	7.80
Gas composition (%V/V, dry) carbon dioxide oxygen nitrogen	4.10 16.40 79.50	4.00 16.50 79.50	4.80 15.90 79.30
Isokinetic variation (%)	98.6	100.3	100.8
Particulate concentration actual standard (GR/ACF) (GR/DSCF)	.0148 .0242	.0100 .0164	.00887 .0148
Part. emission rate (LB/HR)	3.44	2.30	2.00

Note: Dry + Organic/Inorganic Wet Catch

Table 5b Summary of the Results of the June 8, 1994 Particulate Emission Compliance Test on the Line 2 Konus Stack at the Louisiana Pacific Corporation Plant Located in Hayward, Wisconsin.

ITEM	Run 1	Run 2	Run 3
Date of test	06-08-94	06-08-94	06-08-94
Time runs were done (HRS)	757/ 858	920/1021	1114/1215
Volumetric flow actual (ACFM) standard (DSCFM)	27063 16583	26771 16372	26291 15772
Gas temperature (DEG-F)	319	317	325
Moisture content (%V/V)	6.60	6.99	7.80
Gas composition (%V/V, dry) carbon dioxide oxygen nitrogen	4.10 16.40 79.50	4.00 16.50 79.50	4.80 15.90 79.30
Isokinetic variation (%)	98.6	100.3	100.8
Particulate concentration actual (GR/ACF) standard (GR/DSCF)	.0113 .0185	.00681 .0111	.00654 .0109
Part. emission rate (LB/HR)	2.62	1.56	1.47

Note: Dry Catch Only

Table 6.a Summary of the Results of the June 9, 1994 Particulate Emission Compliance Test on the Line 2 Press RTO Inlet at the Louisiana Pacific Corporation Plant Located in Hayward, Wisconsin.

ITEM	Run 1	Run 2	Run 3
Date of test	06-09-94	06-09-94	06-09-94
Time runs were done (HRS)	1240/1345	1425/1530	1605/1708
Volumetric flow actual standard (ACFM) (DSCFM)	98275 82705	101098 85694	104155 88252
Gas temperature (DEG-F)	118	121	120
Moisture content (%V/V)	2.46	2.37	2.58
Gas composition (%V/V, dry) carbon dioxide oxygen nitrogen	0.03 20.90 79.07	0.03 20.90 79.07	0.03 20.90 79.07
Isokinetic variation (%)	98.7	99.0	99.4
Particulate concentration actual standard (GR/ACF) (GR/DSCF)	0.136 0.161	.0918 0.108	0.118 0.139
Part. emission rate (LB/HR)	114.4	79.62	105.5

Note: Dry + Organic/Inorganic Wet Catch

Table 6b Summary of the Results of the June 9, 1994 Particulate Emission Compliance Test on the Line 2 Press RTO Inlet at the Louisiana Pacific Corporation Plant Located in Hayward, Wisconsin.

ITEM	Run 1	Run 2	Run 3
Date of test	06-09-94	06-09-94	06-09-94
Time runs were done (HRS)	1240/1345	1425/1530	1605/1708
Volumetric flow actual standard (ACFM) (DSCFM)	98275 82705	101098 85694	104155 88252
Gas temperature (DEG-F)	118	121	120
Moisture content (%V/V)	2.46	2.37	2.58
Gas composition (%V/V, dry) carbon dioxide oxygen nitrogen	0.03 20.90 79.07	0.03 20.90 79.07	0.03 20.90 79.07
Isokinetic variation (%)	98.7	99.0	99.4
Particulate concentration actual standard (GR/ACF) (GR/DSCF)	0.133 0.158	.0817 .0964	0.116 0.137
Part. emission rate (LB/HR)	111.7	70.82	103.5

Note: Dry Catch Only

Table 7a. Summary of the Results of the June, 1994 **Oxides of Nitrogen** Emission Compliance Tests at the Louisiana Pacific OSB Plant in Hayward, Wisconsin.

<u>Date</u>	<u>Time (HRS)</u>	<u>Concentration (ppm,d)</u>	<u>Emission Rate (LB/HR)</u>
(Line 1 Press RTO Stack)			
6-10-94	0935-1036	25	12.3
6-10-94	1100-1201	17	7.9
6-10-94	1220-1321	15	6.9
Avg		19	9.0
(Line 2 Press RTO Stack)			
6-08-94	1240-1342	14	8.3
6-08-94	1425-1527	12	7.0
6-08-94	1605-1719	8	4.8
Avg		11	6.7

Table 7b. Summary of the Results of the June, 1994 Oxides of Nitrogen Emission Compliance Tests at the Louisiana Pacific OSB Plant in Hayward, Wisconsin.

	Time	Concentration	Emission Factor	Emission Rate
Date	(HRS)	(ppm,d)	(LB/10 ⁶ BTU)	(LB/HR)
(Line 1 Konus Stack)				
6-08-94	1538-1640	78	0.292	5.97
6-08-94	1708-1811	80	0.355	6.42
6-08-94	1835-1938	70	0.227	5.46
Avg		76	0.291	5.95
(Line 2 Konus Stack)				
6-08-94	0757-0858	57	0.304	6.72
6-08-94	0920-1021	58	0.316	6.81
6-08-94	1114-1215	73	0.350	8.19
Avg		63	0.323	7.24

Table 8a. Summary of the Results of the June, 1994 Carbon Monoxide Emission Compliance Tests at the Louisiana Pacific OSB Plant in Hayward, Wisconsin.

	Time	Concentration	Emission Rate
Date	(HRS)	(ppm,d)	(LB/HR)
(Line 1 Press RTO Stack)			
6-10-94	0935-1036	17	5.1
6-10-94	1100-1201	10	2.8
6-10-94	1220-1321	9	2.5
Avg.		12	3.5
(Line 2 Press RTO Stack)			
6-09-94	1240-1342	9	3.2
6-09-94	1425-1527	13	4.5
6-09-94	1605-1719	23	4.0
Avg.		15	3.9

Table 8b. Summary of the June, 1994 **Carbon Monoxide** Emission Compliance Tests at the Louisiana Pacific OSB Plant in Hayward, Wisconsin.

Date	Time (HRS)	Concentration (ppm,d)	Emission Factor (LB/10 ⁶ BTU)	Emission Rate (LB/HR)	
(Line 1 Konus Stack) - Malfunction during Run 3					
6-08-94	1538-1640	92	0.210	4.32	
6-08-94	1708-1811	90	0.243	4.42	
6-08-94	1835-1935	704	1.39	33.6	
Avg.		295	0.613	14.1	23 mm
6-09-94	1345-1606	61	0.139	2.93	
6-09-94	1632-1743	179	0.353	8.40	
6-06-94	1802-1904	53	0.115	2.52	
Avg.		98	0.202	4.62	22.9
(Test used for <u>compliance</u> demonstration)					
6-09-94	0851-1052	105	0.278	4.96	
6-09-94	1240-1534	104	0.253	4.84	
6-09-94	1610-1812	135	0.277	6.42	
Avg.		115	0.269	5.41	20.1
(Line 2 Konus Stack)					
6-08-94	0757-0858	73	0.237	5.28	
6-08-94	0920-1021	67	0.222	4.78	
6-08-94	1114-1215	62	0.181	4.27	
Avg.		67	0.213	4.78	22.44

Table 9. Summary of the June, 1994 **Formaldehyde** Emission Compliance Tests at the Louisiana Pacific OSB Plant in Hayward, Wisconsin.

Date	Time (HRS)	Concentration (ppm,d)	Emission Rate (LB/HR)
(Line 1 Press RTO Stack)			
6-07-94	1250-1352	0.24	0.075
6-07-94	1420-1522	0.01	0.002
6-07-94	1545-1646	0.33	0.105
Avg.		0.19	0.061
(Line 2 Press RTO Stack)			
6-10-94	0815-0918	0.24	0.089
6-10-94	0941-1043	0.20	0.076
6-10-94	1121-1333	0.22	0.081
Avg.		0.22	0.082
(Line 1 Konus Stack)			
6-09-94	1345-1606	0.03	0.0017
6-09-94	1632-1743	0.08	0.0042
6-09-94	1802-1904	0.05	0.0024
Avg.		0.05	0.0028
(Line 2 Konus Stack)			
06-08-94	1446-1553	0.05	0.0041
06-08-94	1616-1718	0.04	0.0029
06-08-94	1742-1843	0.07	0.0061
Avg		0.05	0.0044

Table 10. Summary of the June, 1994 MDI Emission Compliance Tests at the Louisiana Pacific OSB Plant in Hayward, Wisconsin.

Date	Time (HRS)	Concentration (ppm,d)	Emission Rate (LB/HR)
(Line 1 Press RTO Stack)			
6-08-94	0815-0916	0.0005	0.001
6-08-94	0945-1046	< 0.0002	< 0.0006
6-08-94	1115-1216	0.0005	0.001
Avg.		≤ 0.0004	≤ 0.001
(Line 2 Press RTO Stack)			
6-09-94	1325-1441	0.0007	0.002
6-09-94	1518-1641	< 0.0002	< 0.0008
6-09-94	1712-1828	0.0006	0.002
Avg.		≤ 0.0005	≤ 0.002

Table 11. Summary of the June, 1994 **Phenol** Emission Compliance Tests at the Louisiana Pacific OSB Plant in Hayward, Wisconsin.

Date	Time (HRS)	Concentration (ppb.d)	Emission Rate (10 ⁻³ LB/HR)
(Line 1 Konus Stack)			
6-09-94	0845-0945	< 175	< 28
6-09-94	1000-1100	< 175	< 27
6-09-94	1111-1320	< 176	< 28
Avg.		< 175	< 28
(Line 2 Konus Stack)			
6-08-94	1447-1554	< 176	< 42
6-08-94	1616-1718	< 177	< 41
6-08-94	1743-1844	< 176	< 45
Avg.		< 176	< 43

Table 12a. Summary of the June 9 & 10, 1994 Total Hydrocarbon Emission Compliance Tests at the Louisiana Pacific Plant in Hayward, Wisconsin.

Date	Time (HRS)	Concentration (ppmC,w)	Emission Rate (LB/HR)
(Line 1 RTO Press Inlet)			
6-10-94	0935-1037	96	11
6-10-94	1100-1205	55	6.5
6-10-94	1220-1322	42	4.9
Avg.		64	7.5
(Line 1 RTO Press Stack)			
6-10-94	0935-1036	3	0.40
6-10-94	1100-1201	3	0.37
6-10-94	1220-1321	2	0.31
Avg.		3	0.36
(Line 2 Press RTO Inlet)			
6-09-94	1240-1345	89	14
6-09-94	1425-1530	52	8.5
6-09-94	1605-1708	54	9.1
Avg.		65	10.5
(Line 2 Press RTO Stack)			
6-09-94	1240-1345	1.7	0.27
6-09-94	1425-1530	1.5	0.24
6-09-94	1605-1708	1.6	0.24
Avg.		1.6	0.25

Table 12b. Summary of the Results of the June 9 & 10, 1994 **Total Hydrocarbon Removal Efficiency Tests** at the Louisiana Pacific Corporation Plant in Hayward, Wisconsin.

	Time	THC Emission Rate (LB/HR)		Removal
Date	(HRS)	(Inlet)	(Stack)	Efficiency
				(%)
(Line 1 Press RTO)				
6-10-94	0935-1037	11	0.40	96
6-10-94	1100-1205	7	0.37	95
6-10-94	1220-1322	5	0.31	94
Average				95
(Line 2 Press RTO)				
6-09-94	1240-1435	14	0.27	98
6-09-94	1425-1530	9	0.24	97
6-09-94	1605-1708	9	0.24	97
Average				97

Table 14. Summary of the June, 1994 Benzene Emission Compliance Tests at the Louisiana Pacific OSB Plant in Hayward, Wisconsin.

Date	Time (HRS)	Concentration (ppm,d)	Emission Rate (LB/HR)
(Line 1 Korus Stack)			
6-09-94	0845-0945	< 0.0115	< 0.00153
6-09-94	1000-1100	< 0.0111	< 0.00144
6-09-94	1111-1320	< 0.0115	< 0.00152
Avg.		< 0.0114	< 0.00150
(Line 2 Korus Stack)			
6-07-94	0849-0951	< 0.0106	< 0.00230
6-07-94	1142-1242	< 0.0112	< 0.00243
6-07-94	1436-1536	< 0.0113	< 0.00248
Avg.		< 0.0110	< 0.00240

Table 15 Summary of the Results of the June 9, 1994 Polycyclic Organic Matter Determination on the Line 1 Konus Stack at the Louisiana Pacific Corporation Plant Located in Hayward, Wisconsin.

Item	RUN 1	RUN 2	RUN 3
(Concentration ug/Nm ³)			
Benzo-a-anthracene	.75<	3.9	4.4
Benzo-b-fluoranthene	21	11	14
Benzo-a-pyrene	5.4	.5<	3.9
Dibenzo-a,h-anthracene	.36<	.36<	.36<
Dibenzo-a,i-pyrene	8.3<	8.3<	8.1<
Dibenzo-a,h-acridine	6.2<	6.2<	6.1<
Dibenzo-a,j-acridine	.66<	.66<	.65<
7H-Dibenzo-c,g-carbazole	.5<	.5<	.49<
Dibenzo-a,h-pyrene	8.3<	8.3<	8.1<
Indeno (1-2-3-cd)pyrene	2.9	.95	1.5
(Emission Rate 10 ⁻⁶ g/sec)			
Benzo-a-anthracene	3.8<	20	23
Benzo-b-fluoranthene	109	54	71
Benzo-a-pyrene	28	2.5<	20
Dibenzo-a,h-anthracene	1.9<	1.8<	1.8<
Dibenzo-a,i-pyrene	43<	42<	42<
Dibenzo-a,h-acridine	32<	31<	31<
Dibenzo-a,j-acridine	3.4<	3.3<	3.3<
7H-Dibenzo-c,g-carbazole	2.6<	2.5<	2.5<
Dibenzo-a,h-pyrene	43<	42<	42<
Indeno (1-2-3-cd)pyrene	15	4.8	7.9

Table 16 Summary of the Results of the June 9, 1994 Polycyclic Organic Matter Determination on the Line 2 Konus Stack at the Louisiana Pacific Corporation Plant Located in Hayward, Wisconsin.

Item	RUN 1	RUN 2	RUN 3
(Concentration ug/Nm ³)			
Benzo-a-anthracene	.6<	.6<	.59<
Benzo-b-fluoranthene	.33<	.33<	.32<
Benzo-a-pyrene	1.6	.4<	.39<
Dibenzo-a,h-anthracene	.29<	.29<	.29<
Dibenzo-a,i-pyrene	6.6<	6.6<	6.5<
Dibenzo-a,h-acridine	5<	5<	4.9<
Dibenzo-a,j-acridine	.53<	.53<	.52<
7H-Dibenzo-c,g-carbazole	.4<	.4<	.39<
Dibenzo-a,h-pyrene	6.6<	6.6<	6.5<
Indeno (1-2-3-cd)pyrene	.3<	.3<	.29<
(Emission Rate 10 ⁻⁶ g/sec)			
Benzo-a-anthracene	5.0<	5.0<	5.0<
Benzo-b-fluoranthene	2.8<	2.8<	2.8<
Benzo-a-pyrene	14	3.4<	3.3<
Dibenzo-a,h-anthracene	2.5<	2.5<	2.5<
Dibenzo-a,i-pyrene	56<	56<	56<
Dibenzo-a,h-acridine	42<	42<	42<
Dibenzo-a,j-acridine	4.5<	4.5<	4.5<
7H-Dibenzo-c,g-carbazole	3.4<	3.4<	3.3<
Dibenzo-a,h-pyrene	56<	56<	56<
Indeno (1-2-3-cd)pyrene	2.5<	2.5<	2.5<

3 RESULTS

The results of all field and laboratory evaluations are presented in this section. Gas composition (orsat and moisture) are presented first followed by the computer printout of the particulate, oxides of nitrogen, opacity, carbon monoxide, formaldehyde, MDI, phenol, and PAH results. Preliminary measurements including test port locations are given in the appendices.

The results have been calculated on a personal computer using programs written in Extended BASIC specifically for source testing calculations. EPA-published equations have been used as the basis of the calculation techniques in these programs. The emission rates have been calculated using the product of the concentration times flow method.

3.1 Results of Orsat and Moisture Determinations

Test No. 1
Line 1 Press RTO Outlet Stack

Results of Orsat & Moisture Analyses-----Methods 3 & 4(%v/v)

	Run 1	Run 2	Run 3
Date of run	06-07-94	06-07-94	06-07-94

Dry basis (orsat)

carbon dioxide.....	0.30	0.40	0.40
oxygen.....	20.50	20.50	20.50
nitrogen.....	79.20	79.10	79.10

Wet basis (orsat)

carbon dioxide.....	0.29	0.39	0.39
oxygen.....	20.04	20.06	19.90
nitrogen.....	77.42	77.42	76.77
water vapor.....	2.25	2.12	2.95
Dry molecular weight.....	28.87	28.88	28.88
Wet molecular weight.....	28.62	28.65	28.56
Specific gravity.....	0.989	0.990	0.987
Water mass flow.....(LB/HR)	0.00	0.00	0.00

FO	1.333	1.000	1.000
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Test No. 2
Line 1 Press RTO Outlet Stack

Results of Orsat & Moisture Analyses-----Methods 3 & 4(%v/v)

Date of run	Run 1 06-08-94	Run 2 06-08-94	Run 3 06-08-94
Dry basis (orsat)			
carbon dioxide.....	0.40	0.40	0.40
oxygen.....	20.60	20.60	20.60
nitrogen.....	79.00	79.00	79.00
Wet basis (orsat)			
carbon dioxide.....	0.39	0.39	0.39
oxygen.....	19.93	19.91	20.01
nitrogen.....	76.43	76.35	76.75
water vapor.....	3.25	3.36	2.84
Dry molecular weight.....	28.89	28.89	28.89
Wet molecular weight.....	28.53	28.52	28.58
Specific gravity.....	0.986	0.985	0.987
Water mass flow.....(LB/HR)	0.00	0.00	0.00
FO	0.750	0.750	0.750

Test No. 3
Line 1 Press RTO Outlet Stack

Results of Orsat & Moisture Analyses-----Methods 3 & 4(%v/v)

Date of run	Run 1 06-10-94	Run 2 06-10-94	Run 3 06-10-94
Dry basis (orsat)			
carbon dioxide.....	0.40	0.40	0.40
oxygen.....	20.50	20.50	20.50
nitrogen.....	79.10	79.10	79.10
Wet basis (orsat)			
carbon dioxide.....	0.39	0.39	0.39
oxygen.....	20.00	19.87	19.90
nitrogen.....	77.16	76.68	76.78
water vapor.....	2.45	3.06	2.93
Dry molecular weight.....	28.88	28.88	28.88
Wet molecular weight.....	28.62	28.55	28.57
Specific gravity.....	0.989	0.986	0.987
Water mass flow.....(LB/HR)	4821	5843	5598
FO	1.000	1.000	1.000

Test No. 5
Line 1 Press RTO Inlet

Results of Orsat & Moisture Analyses-----Methods 3 & 4(%v/v)

	Run 1	Run 2	Run 3
Date of run	06-10-94	06-10-94	06-10-94

Dry basis (orsat)

carbon dioxide.....	0.03	0.03	0.03
oxygen.....	20.90	20.90	20.90
nitrogen.....	79.07	79.07	79.07

Wet basis (orsat)

carbon dioxide.....	0.03	0.03	0.03
oxygen.....	20.50	20.38	20.42
nitrogen.....	77.56	77.12	77.25
water vapor.....	1.92	2.46	2.30
Dry molecular weight.....	28.84	28.84	28.84
Wet molecular weight.....	28.63	28.57	28.59
Specific gravity.....	0.989	0.987	0.988
Water mass flow.....(LB/HR)	3353	4375	4045

Test No. 5
Line 1 Konus Stack

Results of Orsat & Moisture Analyses-----Methods 3 & 4(%v/v)

Date of run	Run 1 06-08-94	Run 2 06-08-94	Run 3 06-08-94
Dry basis (orsat)			
carbon dioxide.....	6.00	5.00	7.00
oxygen.....	14.50	15.50	13.50
nitrogen.....	79.50	79.50	79.50
Wet basis (orsat)			
carbon dioxide.....	5.42	4.57	6.24
oxygen.....	13.09	14.17	12.03
nitrogen.....	71.79	72.70	70.85
water vapor.....	9.70	8.55	10.88
Dry molecular weight.....	29.54	29.42	29.66
Wet molecular weight.....	28.42	28.44	28.39
Specific gravity.....	0.982	0.983	0.981
Water mass flow.....(LB/HR)	3244	2955	3744
FO	1.067	1.080	1.057

Test No. 6
Line 1 Konus Stack

Results of Orsat & Moisture Analyses-----Methods 3 & 4(%v/v)

	Run 1	Run 2	Run 3
Date of run	06-09-94	06-09-94	06-09-94

Dry basis (orsat)

carbon dioxide.....	6.20	7.10	6.50
oxygen.....	14.50	13.50	14.20
nitrogen.....	79.30	79.40	79.30

Wet basis (orsat)

carbon dioxide.....	5.72	6.43	5.94
oxygen.....	13.39	12.23	12.99
nitrogen.....	73.21	71.96	72.53
water vapor.....	7.68	9.37	8.54
Dry molecular weight.....	29.57	29.68	29.61
Wet molecular weight.....	28.68	28.58	28.62
Specific gravity.....	0.991	0.987	0.988
Water mass flow.....(LB/HR)	0.00	0.00	0.00

FO	1.032	1.042	1.031
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Test No. 8
Line 1 Konus Stack

Results of Orsat & Moisture Analyses-----Methods 3 & 4(%v/v)

Date of run	Run 1 06-09-94	Run 2 06-09-94	Run 3 06-09-94
Dry basis (orsat)			
carbon dioxide.....	5.30	5.90	6.90
oxygen.....	15.40	14.90	13.80
nitrogen.....	79.30	79.20	79.30
Wet basis (orsat)			
carbon dioxide.....	4.87	5.40	6.22
oxygen.....	14.16	13.63	12.43
nitrogen.....	72.90	72.46	71.44
water vapor.....	8.07	8.52	9.91
Dry molecular weight.....	29.46	29.54	29.66
Wet molecular weight.....	28.54	28.56	28.50
Specific gravity.....	0.986	0.986	0.984
Water mass flow.....(LB/HR)	0.00	0.00	0.00
FO	1.038	1.017	1.029

Test No. 12
Line 2 Press RTO Outlet Stack

Results of Orsat & Moisture Analyses-----Methods 3 & 4(%v/v)

	Run 1	Run 2	Run 3
Date of run	06-10-94	06-10-94	06-10-94

Dry basis (orsat)

carbon dioxide.....	0.40	0.40	0.40
oxygen.....	20.55	20.60	20.55
nitrogen.....	79.05	79.00	79.05

Wet basis (orsat)

carbon dioxide.....	0.39	0.39	0.39
oxygen.....	20.01	20.08	20.17
nitrogen.....	76.99	77.01	77.57
water vapor.....	2.61	2.52	1.87
Dry molecular weight.....	28.89	28.89	28.89
Wet molecular weight.....	28.60	28.61	28.68
Specific gravity.....	0.988	0.988	0.991
Water mass flow.....(LB/HR)	0.00	0.00	0.00

FO	0.875	0.750	0.875
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Test No. 13
Line 2 Press RTO Outlet Stack

Results of Orsat & Moisture Analyses-----Methods 3 & 4(%v/v)

	Run 1	Run 2	Run 3
Date of run	06-09-94	06-09-94	06-09-94

Dry basis (orsat)

carbon dioxide.....	0.03	0.03	0.03
oxygen.....	20.90	20.90	20.90
nitrogen.....	79.07	79.07	79.07

Wet basis (orsat)

carbon dioxide.....	0.03	0.03	0.03
oxygen.....	20.41	20.37	20.47
nitrogen.....	77.21	77.06	77.45
water vapor.....	2.35	2.54	2.05
Dry molecular weight.....	28.84	28.84	28.84
Wet molecular weight.....	28.59	28.57	28.62
Specific gravity.....	0.987	0.987	0.989
Water mass flow.....(LB/HR)	0.00	0.00	0.00

Test No. 14
Line 2 Press RTO Stack

Results of Orsat & Moisture Analyses-----Methods 3 & 4(%v/v)

	Run 1	Run 2	Run 3
Date of run	06-09-94	06-09-94	06-09-94

Dry basis (orsat)

carbon dioxide.....	0.40	0.40	0.40
oxygen.....	20.60	20.60	20.55
nitrogen.....	79.00	79.00	79.05

Wet basis (orsat)

carbon dioxide.....	0.39	0.39	0.39
oxygen.....	20.11	20.08	20.13
nitrogen.....	77.14	76.99	77.43
water vapor.....	2.35	2.55	2.05
Dry molecular weight.....	28.89	28.89	28.89
Wet molecular weight.....	28.63	28.61	28.66
Specific gravity.....	0.989	0.988	0.990
Water mass flow.....(LB/HR)	5530	5940	4680

FO	0.750	0.750	0.875
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Test No. 16
Line 2 Konus Stack

Results of Orsat & Moisture Analyses-----Methods 3 & 4(%v/v)

	Run 1	Run 2	Run 3
Date of run	06-08-94	06-08-94	06-08-94

Dry basis (orsat)

carbon dioxide.....	4.10	4.00	4.80
oxygen.....	16.40	16.50	15.90
nitrogen.....	79.50	79.50	79.30

Wet basis (orsat)

carbon dioxide.....	3.83	3.72	4.43
oxygen.....	15.32	15.35	14.66
nitrogen.....	74.26	73.94	73.12
water vapor.....	6.60	6.99	7.80
Dry molecular weight.....	29.31	29.30	29.40
Wet molecular weight.....	28.57	28.51	28.51
Specific gravity.....	0.987	0.985	0.985
Water mass flow.....(LB/HR)	3285	3454	3742

FO	1.098	1.100	1.042
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Test No. 17
Line 2 Konus Stack

Results of Orsat & Moisture Analyses-----Methods 3 & 4(%v/v)

	Run 1	Run 2	Run 3
Date of run	06-08-94	06-08-94	06-08-94

Dry basis (orsat)

carbon dioxide.....	4.40	4.40	4.30
oxygen.....	16.60	16.60	16.60
nitrogen.....	79.00	79.00	79.10

Wet basis (orsat)

carbon dioxide.....	4.12	4.13	4.03
oxygen.....	15.55	15.57	15.57
nitrogen.....	74.00	74.08	74.18
water vapor.....	6.33	6.23	6.22
Dry molecular weight.....	29.37	29.37	29.35
Wet molecular weight.....	28.65	28.66	28.65
Specific gravity.....	0.990	0.990	0.990
Water mass flow.....(LB/HR)	0.00	0.00	0.00

FO	0.977	0.977	1.000
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Test No. 19
Line 2 Konus Stack

Results of Orsat & Moisture Analyses-----Methods 3 & 4(%v/v)

	Run 1	Run 2	Run 3
Date of run	06-07-94	06-07-94	06-07-94

Dry basis (orsat)

carbon dioxide.....	5.00	4.90	4.00
oxygen.....	15.80	15.90	16.90
nitrogen.....	79.20	79.20	79.10

Wet basis (orsat)

carbon dioxide.....	4.58	4.51	3.68
oxygen.....	14.49	14.64	15.56
nitrogen.....	72.61	72.92	72.83
water vapor.....	8.32	7.93	7.93
Dry molecular weight.....	29.43	29.42	29.32
Wet molecular weight.....	28.48	28.51	28.42
Specific gravity.....	0.984	0.985	0.982
Water mass flow.....(LB/HR)	0.00	0.00	0.00

FO	1.020	1.020	1.000
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Test No. 21
Line 2 Press RTO Inlet

Results of Orsat & Moisture Analyses-----Methods 3 & 4(%v/v)

	Run 1	Run 2	Run 3
Date of run	06-09-94	06-09-94	06-09-94

Dry basis (orsat)

carbon dioxide.....	0.03	0.03	0.03
oxygen.....	20.90	20.90	20.90
nitrogen.....	79.07	79.07	79.07

Wet basis (orsat)

carbon dioxide.....	0.03	0.03	0.03
oxygen.....	20.39	20.40	20.36
nitrogen.....	77.12	77.20	77.03
water vapor.....	2.46	2.37	2.58

Dry molecular weight.....	28.84	28.84	28.84
Wet molecular weight.....	28.57	28.58	28.56
Specific gravity.....	0.987	0.987	0.987
Water mass flow.....(LB/HR)	5859	5838	6545

3.2 Results of Particulate Determinations

Test No. 5
Line 1 Press RTO Inlet

Results of Particulate Loading Determinations-----Method 5

	Run 1	Run 2	Run 3
Date of run	06-10-94	06-10-94	06-10-94
Time run start/end.....(HRS)	935/1037	1100/1205	1220/1322
Static pressure.....(IN.WC)	-2.95	-2.95	-2.95
Cross sectional area (SQ.FT)	15.39	15.39	15.39
Pitot tube coefficient.....	.840	.840	.840
Water in sample gas			
condenser.....(ML)	0.0	0.0	0.0
impingers.....(GRAMS)	0.0	7.0	2.0
desiccant.....(GRAMS)	19.0	18.0	21.0
total.....(GRAMS)	19.0	25.0	23.0
Total particulate material..			
.....collected(grams)	0.0430	0.0295	0.0387
Gas meter coefficient.....	0.9961	0.9961	0.9961
Barometric pressure..(IN.HG)	28.93	28.93	28.93
Avg. orif.pres.drop..(IN.WC)	1.94	2.04	2.00
Avg. gas meter temp..(DEF-F)	77.5	87.8	91.9
Volume through gas meter....			
at meter conditions...(CF)	48.27	50.02	49.74
standard conditions.(DSCF)	45.88	46.66	46.05
Total sampling time....(MIN)	60.00	60.00	60.00
Nozzle diameter.....(IN)	.188	.188	.188
Avg.stack gas temp ..(DEG-F)	121	123	126
Volumetric flow rate.....			
actual.....(ACFM)	71543	72779	72499
dry standard.....(DSCFM)	61212	61735	61233
Isokinetic variation.....(%)	99.8	100.6	100.1
Particulate concentration...			
actual.....(GR/ACF)	0.01237	0.00827	0.01095
dry standard.....(GR/DSCF)	0.01446	0.00976	0.01297
Particle mass rate...(LB/HR)	7.588	5.162	6.806

Test No. 3
Line 1 Press RTO Outlet Stack

Results of Particulate Loading Determinations-----Method 5

	Run 1 06-10-94	Run 2 06-10-94	Run 3 06-10-94
Date of run			
Time run start/end.....(HRS)	935/1036	1100/1201	1220/1321
Static pressure.....(IN.WC)	-0.43	-0.43	-0.43
Cross sectional area (SQ.FT)	31.09	31.09	31.09
Pitot tube coefficient.....	.840	.840	.840
Water in sample gas			
condenser.....(ML)	0.0	0.0	0.0
impingers.....(GRAMS)	9.0	13.0	14.0
desiccant.....(GRAMS)	15.0	16.0	14.0
total.....(GRAMS)	24.0	29.0	28.0
Total particulate material..			
.....collected(grams)	0.0311	0.0270	0.0221
Gas meter coefficient.....	1.0066	1.0066	1.0066
Barometric pressure..(IN.HG)	28.93	28.93	28.93
Avg. orif.pres.drop..(IN.WC)	1.91	1.85	1.89
Avg. gas meter temp..(DEF-F)	71.5	84.4	90.5
Volume through gas meter....			
at meter conditions...(CF)	46.38	45.67	46.68
standard conditions.(DSCF)	45.04	43.30	43.77
Total sampling time....(MIN)	60.00	60.00	60.00
Nozzle diameter.....(IN)	.251	.251	.251
Avg.stack gas temp ..(DEG-F)	259	264	268
Volumetric flow rate.....			
actual.....(ACFM)	98861	96534	97230
dry standard.....(DSCFM)	68420	65961	66157
Isokinetic variation.....(%)	99.3	99.0	99.8
Particulate concentration...			
actual.....(GR/ACF)	0.00737	0.00657	0.00530
dry standard.....(GR/DSCF)	0.01065	0.00962	0.00779
Particle mass rate...(LB/HR)	6.248	5.440	4.418

Test No. 5
Line 1 Konus Stack

Results of Particulate Loading Determinations-----Method 5

	Run 1 06-08-94	Run 2 06-08-94	Run 3 06-08-94
Date of run			
Time run start/end.....(HRS)	1538/1640	1708/1811	1835/1938
Static pressure.....(IN.WC)	-0.20	-0.20	-0.20
Cross sectional area (SQ.FT)	14.75	14.75	14.75
Pitot tube coefficient.....	.840	.840	.840
Water in sample gas			
condenser.....(ML)	0.0	0.0	0.0
impingers.....(GRAMS)	57.0	51.0	71.0
desiccant.....(GRAMS)	13.0	11.0	10.0
total.....(GRAMS)	70.0	62.0	81.0
Total particulate material..			
.....collected(grams)	0.0743	0.0423	0.0513
Gas meter coefficient.....	0.9974	0.9974	0.9974
Barometric pressure..(IN.HG)	28.98	28.98	28.98
Avg. orif.pres.drop..(IN.WC)	0.88	0.92	0.92
Avg. gas meter temp..(DEF-F)	80.3	86.0	87.5
Volume through gas meter....			
at meter conditions...(CF)	32.50	33.40	33.52
standard conditions.(DSCF)	30.74	31.26	31.29
Total sampling time....(MIN)	60.00	60.00	60.00
Nozzle diameter.....(IN)	.355	.355	.355
Avg.stack gas temp ..(DEG-F)	310	314	314
Volumetric flow rate.....			
actual.....(ACFM)	17975	18652	18575
dry standard.....(DSCFM)	10771	11266	10936
Isokinetic variation.....(%)	102.1	99.3	102.4
Particulate concentration...			
actual.....(GR/ACF)	0.02234	0.01261	0.01489
dry standard.....(GR/DSCF)	0.03730	0.02088	0.02530
Particle mass rate...(LB/HR)	3.443	2.016	2.371

Test No. 16
Line 2 Konus Stack

Results of Particulate Loading Determinations-----Method 5

	Run 1	Run 2	Run 3
Date of run	06-08-94	06-08-94	06-08-94
Time run start/end.....(HRS)	757/ 858	920/1021	1114/1215
Static pressure.....(IN.WC)	-0.28	-0.28	-0.28
Cross sectional area (SQ.FT)	14.47	14.47	14.47
Pitot tube coefficient.....	.840	.840	.840
Water in sample gas			
condenser.....(ML)	0.0	0.0	0.0
impingers.....(GRAMS)	58.0	62.0	67.0
desiccant.....(GRAMS)	15.0	16.0	18.0
total.....(GRAMS)	73.0	78.0	85.0
Total particulate material..			
.....collected(grams)	0.0764	0.0520	0.0454
Gas meter coefficient.....	0.9961	0.9961	0.9961
Barometric pressure...(IN.HG)	28.98	28.98	28.98
Avg. orif.pres.drop...(IN.WC)	2.13	2.19	2.08
Avg. gas meter temp...(DEF-F)	62.5	74.3	80.5
Volume through gas meter....			
at meter conditions...(CF)	49.74	51.03	50.03
standard conditions.(DSCF)	48.74	48.90	47.38
Total sampling time....(MIN)	60.00	60.00	60.00
Nozzle diameter.....(IN)	.363	.363	.363
Avg.stack gas temp ..(DEG-F)	319	317	325
Volumetric flow rate.....			
actual.....(ACFM)	27063	26771	26291
dry standard.....(DSCFM)	16583	16372	15772
Isokinetic variation.....(%)	98.6	100.3	100.8
Particulate concentration...			
actual.....(GR/ACF)	0.01482	0.01003	0.00887
dry standard.....(GR/DSCF)	0.02419	0.01641	0.01478
Particle mass rate...(LB/HR)	3.438	2.302	1.999

Test No. 21
Line 2 Press RTO Inlet

Results of Particulate Loading Determinations-----Method 5

	Run 1	Run 2	Run 3
Date of run	06-09-94	06-09-94	06-09-94
Time run start/end.....(HRS)	1240/1345	1425/1530	1605/1708
Static pressure.....(IN.WC)	-4.40	-4.40	-4.40
Cross sectional area (SQ.FT)	18.67	18.67	18.67
Pitot tube coefficient.....	.840	.840	.840
Water in sample gas			
condenser.....(ML)	0.0	0.0	0.0
impingers.....(GRAMS)	2.0	1.0	2.0
desiccant.....(GRAMS)	22.0	23.0	25.0
total.....(GRAMS)	24.0	24.0	27.0
Total particulate material..			
.....collected(grams)	0.4684	0.3273	0.4352
Gas meter coefficient.....	1.0066	1.0066	1.0066
Barometric pressure..(IN.HG)	28.58	28.90	28.90
Avg. orif.pres.drop..(IN.WC)	2.01	2.17	2.31
Avg. gas meter temp..(DEF-F)	77.4	93.0	95.7
Volume through gas meter....			
at meter conditions...(CF)	47.20	49.93	51.84
standard conditions.(DSCF)	44.80	46.59	48.15
Total sampling time....(MIN)	60.00	60.00	60.00
Nozzle diameter.....(IN)	.177	.177	.177
Avg.stack gas temp ..(DEG-F)	118	121	120
Volumetric flow rate.....			
actual.....(ACFM)	98275	101098	104155
dry standard.....(DSCFM)	82705	85694	88252
Isokinetic variation.....(%)	98.7	99.0	99.4
Particulate concentration...			
actual.....(GR/ACF)	0.13571	0.09185	0.11811
dry standard.....(GR/DSCF)	0.16132	0.10840	0.13945
Particle mass rate...(LB/HR)	114.358	79.622	105.489

Test No. 14
Line 2 Press RTO Stack

Results of Particulate Loading Determinations-----Method 5

	Run 1 06-09-94	Run 2 06-09-94	Run 3 06-09-94
Date of run			
Time run start/end.....(HRS)	1240/1342	1425/1527	1605/1719
Static pressure.....(IN.WC)	-0.98	-0.98	-0.98
Cross sectional area (SQ.FT)	31.71	31.71	31.71
Pitot tube coefficient.....	.840	.840	.840
Water in sample gas			
condenser.....(ML)	0.0	0.0	0.0
impingers.....(GRAMS)	10.0	10.0	9.0
desiccant.....(GRAMS)	16.0	18.0	13.0
total.....(GRAMS)	26.0	28.0	22.0
Total particulate material..			
.....collected(grams)	0.0685	0.0234	0.0342
Gas meter coefficient.....	0.9947	0.9947	0.9947
Barometric pressure..(IN.HG)	28.90	28.90	28.90
Avg. orif.pres.drop..(IN.WC)	2.69	2.70	2.63
Avg. gas meter temp..(DEF-F)	86.7	96.5	101.4
Volume through gas meter....			
at meter conditions...(CF)	54.43	55.03	54.54
standard conditions.(DSCF)	50.83	50.49	49.59
Total sampling time....(MIN)	60.00	60.00	60.00
Nozzle diameter.....(IN)	.246	.246	.246
Avg.stack gas temp ..(DEG-F)	253	256	258
Volumetric flow rate.....			
actual.....(ACFM)	117314	116983	114900
dry standard.....(DSCFM)	81742	80986	79766
Isokinetic variation.....(%)	99.6	99.9	99.6
Particulate concentration...			
actual.....(GR/ACF)	0.01448	0.00495	0.00738
dry standard.....(GR/DSCF)	0.02079	0.00715	0.01064
Particle mass rate...(LB/HR)	14.568	4.964	7.275

3.3 Results of Oxides of Nitrogen Determinations

Test No. 5
Line 1 Konus Stack

Results of Oxides of Nitrogen (NOx) Determinations-----Method 7

	Run 1A	Run 1B	Run 1C	Run 1D
Date of run.....	06-08-94	06-08-94	06-08-94	06-08-94
Time of run.....(HRS)	1540	1552	1614	1632
Flask number.....	19	20	21	22
Volume of flask.....(ML)	2069	2060	2068	2031

Data: time of sampling

flask temperature..(DEG-F)	70.00	70.00	70.00	70.00
bar. press.....(IN.HG)	28.90	28.90	28.90	28.90
flask vacuum.....(IN.HG)	27.33	27.35	27.41	27.40
flask abs. press...(IN.HG)	1.57	1.55	1.49	1.50

Data: Time of Flask Opening

flask temperature..(DEG-F)	72.00	72.00	72.00	72.00
lab. bar. press....(IN.HG)	28.97	28.97	28.97	28.97
flask static press.(IN.HG)	-0.40	-0.90	-3.20	-0.30
flask abs. press...(IN.HG)	28.57	28.07	25.77	28.67
Volume gas sampled....(DSML)	1830	1789	1644	1807
Moisture content.....(%V/V)	9.70	9.70	9.70	9.70
Nitrate in gas sample...(JG)	359.0	349.0	353.0	347.0
NO2 in gas sample.....(JG)	266.4	259.0	261.9	257.5

NOx Concentration

(GR/DSCF).....	0.0636	0.0633	0.0696	0.0623
(MG/DSCM).....	146	145	159	143
(PPM-DRY).....	76	76	83	75
(PPM-WET).....	69	68	75	67
NOX Emission rate....(LB/HR)	5.87	5.84	6.43	5.75

Test No. 5
Line 1 Konus Stack

Results of Oxides of Nitrogen (NOx) Determinations-----Method 7

	Run 2A	Run 2B	Run 2C	Run 2D
Date of run.....	06-08-94	06-08-94	06-08-94	06-08-94
Time of run.....(HRS)	1708	1723	1738	1755
Flask number.....	23	24	61	62
Volume of flask.....(ML)	2056	2031	2100	2079
Data: time of sampling				
flask temperature..(DEG-F)	70.00	70.00	70.00	70.00
bar. press.....(IN.HG)	28.90	28.90	28.90	28.90
flask vacuum.....(IN.HG)	27.39	27.28	27.50	27.44
flask abs. press...(IN.HG)	1.51	1.62	1.40	1.46
Data: Time of Flask Opening				
flask temperature..(DEG-F)	72.00	72.00	72.00	72.00
lab. bar. press....(IN.HG)	28.97	28.97	28.97	28.97
flask static press.(IN.HG)	-1.00	-0.10	-0.80	-2.40
flask abs. press...(IN.HG)	27.97	28.87	28.17	26.57
Volume gas sampled....(DSML)	1782	1812	1841	1710
Moisture content.....(%V/V)	8.55	8.55	8.55	8.55
Nitrate in gas sample...(JG)	368.0	461.0	313.0	324.0
NO2 in gas sample.....(JG)	273.0	342.1	232.2	240.4
<u>NOx Concentration</u>				
(GR/DSCF).....	0.0670	0.0825	0.0551	0.0614
(MG/DSCM).....	153	189	126	141
(PPM-DRY).....	80	99	66	74
(PPM-WET).....	73	90	60	67
NOX Emission rate....(LB/HR)	6.47	7.97	5.32	5.93

Test No. 5
Line 1 Konus Stack

Results of Oxides of Nitrogen (NOx) Determinations-----Method 7

	Run 3A	Run 3B	Run 3C	Run 3D
Date of run.....	06-08-94	06-08-94	06-08-94	06-08-94
Time of run.....(HRS)	1835	1850	1910	1925
Flask number.....	63	64	65	66
Volume of flask.....(ML)	2067	2087	2068	2096
Data: time of sampling				
flask temperature..(DEG-F)	70.00	70.00	70.00	70.00
bar. press.....(IN.HG)	28.90	28.90	28.90	28.90
flask vacuum.....(IN.HG)	27.43	27.40	27.44	27.50
flask abs. press...(IN.HG)	1.47	1.50	1.46	1.40
Data: Time of Flask Opening				
flask temperature..(DEG-F)	72.00	72.00	72.00	72.00
lab. bar. press....(IN.HG)	28.97	28.97	28.97	28.97
flask static press.(IN.HG)	-2.80	-0.60	-2.00	-1.60
flask abs. press...(IN.HG)	26.17	28.37	26.97	27.37
Volume gas sampled....(DSML)	1672	1837	1728	1783
Moisture content.....(%V/V)	10.88	10.88	10.88	10.88
Nitrate in gas sample...(JG)	352.0	283.0	291.0	331.0
NO2 in gas sample.....(JG)	261.2	210.0	215.9	245.6
<u>NOx Concentration</u>				
(GR/DSCF).....	0.0683	0.0500	0.0546	0.0602
(MG/DSCM).....	156	114	125	138
(PPM-DRY).....	82	60	65	72
(PPM-WET).....	73	53	58	64
NOX Emission rate....(LB/HR)	6.40	4.68	5.12	5.64

Test No. 16
Line 2 Konus Stack

Results of Oxides of Nitrogen (NOx) Determinations-----Method 7

	Run 1A	Run 1B	Run 1C	Run 1D
Date of run.....	06-08-94	06-08-94	06-08-94	06-08-94
Time of run.....(HRS)	800	815	830	845
Flask number.....	13	14	15	16
Volume of flask.....(ML)	2060	2048	2045	2067
Data: time of sampling				
flask temperature..(DEG-F)	59.00	59.00	59.00	60.00
bar. press.....(IN.HG)	28.98	28.98	28.98	28.98
flask vacuum.....(IN.HG)	27.40	27.30	27.40	27.40
flask abs. press...(IN.HG)	1.58	1.68	1.58	1.58
Data: Time of Flask Opening				
flask temperature..(DEG-F)	72.00	72.00	72.00	72.00
lab. bar. press....(IN.HG)	28.97	28.97	28.97	28.97
flask static press.(IN.HG)	0.00	0.40	0.40	-0.30
flask abs. press...(IN.HG)	28.97	29.37	29.37	28.67
Volume gas sampled....(DSML)	1846	1855	1859	1832
Moisture content.....(%V/V)	6.60	6.60	6.60	6.60
Nitrate in gas sample...(JG)	264.0	272.0	272.0	270.0
NO2 in gas sample.....(JG)	195.9	201.8	201.8	200.3
<u>NOx Concentration</u>				
(GR/DSCF).....	0.0464	0.0476	0.0475	0.0478
(MG/DSCM).....	106	109	109	109
(PPM-DRY).....	55	57	57	57
(PPM-WET).....	52	53	53	53
NOX Emission rate....(LB/HR)	6.59	6.76	6.74	6.79

Test No. 16
Line 2 Konus Stack

Results of Oxides of Nitrogen (NOx) Determinations-----Method 7

	Run 2A	Run 2B	Run 2C	Run 2D
Date of run.....	06-08-94	06-08-94	06-08-94	06-08-94
Time of run.....(HRS)	920	935	950	1005
Flask number.....	17	18	55	56
Volume of flask.....(ML)	2054	2045	2086	2069

Data: time of sampling

flask temperature..(DEG-F)	60.00	60.00	60.00	60.00
bar. press.....(IN.HG)	28.98	28.98	28.98	28.98
flask vacuum.....(IN.HG)	27.30	27.30	27.30	27.30
flask abs. press...(IN.HG)	1.68	1.68	1.68	1.68

Data: Time of Flask Opening

flask temperature..(DEG-F)	72.00	72.00	72.00	72.00
lab. bar. press....(IN.HG)	28.97	28.97	28.97	28.97
flask static press.(IN.HG)	-0.90	0.40	0.20	0.00
flask abs. press...(IN.HG)	28.07	29.37	29.17	28.97
Volume gas sampled....(DSML)	1773	1852	1876	1847
Moisture content.....(%V/V)	6.99	6.99	6.99	6.99
Nitrate in gas sample...(JG)	273.0	252.0	283.0	291.0
NO2 in gas sample.....(JG)	202.6	187.0	210.0	215.9

NOx Concentration

(GR/DSCF).....	0.0499	0.0441	0.0489	0.0511
(MG/DSCM).....	114	101	112	117
(PPM-DRY).....	60	53	59	61
(PPM-WET).....	56	49	54	57
NOX Emission rate....(LB/HR)	7.01	6.19	6.86	7.17

Test No. 16
Line 2 Konus Stack

Results of Oxides of Nitrogen (NOx) Determinations-----Method 7

	Run 3A	Run 3B	Run 3C	Run 3D
Date of run.....	06-08-94	06-08-94	06-08-94	06-08-94
Time of run.....(HRS)	1115	1130	1145	1200
Flask number.....	57	58	59	60
Volume of flask.....(ML)	2062	2085	2077	2066

Data: time of sampling

flask temperature..(DEG-F)	64.00	65.00	65.00	65.00
bar. press.....(IN.HG)	28.98	28.98	28.98	28.98
flask vacuum.....(IN.HG)	27.30	27.20	27.30	27.30
flask abs. press...(IN.HG)	1.68	1.78	1.68	1.68

Data: Time of Flask Opening

flask temperature..(DEG-F)	72.00	72.00	72.00	72.00
lab. bar. press....(IN.HG)	28.97	28.97	28.97	28.97
flask static press.(IN.HG)	0.10	-0.40	0.00	-0.30
flask abs. press...(IN.HG)	29.07	28.57	28.97	28.67
Volume gas sampled....(DSML)	1848	1828	1855	1825
Moisture content.....(%V/V)	7.80	7.80	7.80	7.80
Nitrate in gas sample...(JG)	320.0	325.0	340.0	389.0
NO2 in gas sample.....(JG)	237.4	241.1	252.3	288.6

NOx Concentration

(GR/DSCF).....	0.0561	0.0576	0.0594	0.0691
(MG/DSCM).....	128	132	136	158
(PPM-DRY).....	67	69	71	83
(PPM-WET).....	62	64	66	76
NOX Emission rate....(LB/HR)	7.59	7.79	8.03	9.34

3.4 Results of Opacity Observations

Test No. 3
Line 1 Press RTO Outlet Stack

Results of Opacity Observations ----- EPA Method 9

PERCENT OPACITY	OPTICAL DENSITY	RELATIVE FREQUENCY (%)
0	0.0000	100.00
5	0.0223	0.00
10	0.0458	0.00
15	0.0706	0.00
20	0.0969	0.00
25	0.1249	0.00
30	0.1549	0.00
35	0.1871	0.00
40	0.2219	0.00
45	0.2596	0.00
50	0.3010	0.00
55	0.3468	0.00
60	0.3979	0.00
65	0.4559	0.00
70	0.5229	0.00
75	0.6021	0.00
80	0.6690	0.00
85	0.8239	0.00
90	1.0000	0.00
95	1.3010	0.00
99	2.0000	0.00
Avg Opac 0.00	Avg OD 0.0000	Time average

Observer: David Vaaler
Cert. Date: 04-06-94
Date of Observation: 06-10-94
Time of Observation: 1100/1200

Test No. 5
Line 1 Konus Stack

Results of Opacity Observations ----- EPA Method 9

PERCENT OPACITY	OPTICAL DENSITY	RELATIVE FREQUENCY (%)
0	0.0000	100.00
5	0.0223	0.00
10	0.0458	0.00
15	0.0706	0.00
20	0.0969	0.00
25	0.1249	0.00
30	0.1549	0.00
35	0.1871	0.00
40	0.2219	0.00
45	0.2596	0.00
50	0.3010	0.00
55	0.3468	0.00
60	0.3979	0.00
65	0.4559	0.00
70	0.5229	0.00
75	0.6021	0.00
80	0.6690	0.00
85	0.8239	0.00
90	1.0000	0.00
95	1.3010	0.00
99	2.0000	0.00
Avg Opac 0.00	Avg OD 0.0000	Time average

Observer: Edward Juers
Cert. Date: 04-06-94
Date of Observation: 06-08-94
Time of Observation: 1538/1638

Test No. 14
Line 2 Press RTO Outlet Stack

Results of Opacity Observations ----- EPA Method 9

PERCENT OPACITY	OPTICAL DENSITY	RELATIVE FREQUENCY (%)
0	0.0000	100.00
5	0.0223	0.00
10	0.0458	0.00
15	0.0706	0.00
20	0.0969	0.00
25	0.1249	0.00
30	0.1549	0.00
35	0.1871	0.00
40	0.2219	0.00
45	0.2596	0.00
50	0.3010	0.00
55	0.3468	0.00
60	0.3979	0.00
65	0.4559	0.00
70	0.5229	0.00
75	0.6021	0.00
80	0.6690	0.00
85	0.8239	0.00
90	1.0000	0.00
95	1.3010	0.00
99	2.0000	0.00
Avg Opac 0.00	Avg OD 0.0000	Time average

Observer: Edward Juers
Cert. Date: 04-06-94
Date of Observation: 06-09-94
Time of Observation: 1240/0140

Test No. 16
Line 2 Konus Stack

Results of Opacity Observations ----- EPA Method 9

PERCENT OPACITY	OPTICAL DENSITY	RELATIVE FREQUENCY (%)
0	0.0000	80.83
5	0.0223	19.17
10	0.0458	0.00
15	0.0706	0.00
20	0.0969	0.00
25	0.1249	0.00
30	0.1549	0.00
35	0.1871	0.00
40	0.2219	0.00
45	0.2596	0.00
50	0.3010	0.00
55	0.3468	0.00
60	0.3979	0.00
65	0.4559	0.00
70	0.5229	0.00
75	0.6021	0.00
80	0.6690	0.00
85	0.8239	0.00
90	1.0000	0.00
95	1.3010	0.00
99	2.0000	0.00
Avg Opac 0.96	Avg OD 0.0043	Time average

Observer: Edward Juers
Cert. Date: 04-06-94
Date of Observation: 06-08-94
Time of Observation: 0920/1021

3.5 Results of Carbon Monoxide Determinations

Test No. 3
Line 1 Press RTO Outlet Stack

Results of CO Determinations -----Method 10

	Run 1	Run 2	Run 3
Date of run	06-10-94	06-10-94	06-10-94
Time run start/end.....(HRS)	0935/1036	1100/1201	1220/1321
Total sampling time....(MIN)	60.0	60.0	60.0
Moisture content.....(%V/V)	2.45	3.06	2.93
O2 Concentration.....(%V/V)	20.50	20.50	20.50
Volumetric flow rate (DSCFM)	68420	65961	66157
CO concentration.....			
(GR/DSCF).....	0.0088	0.0049	0.0044
(MG/DSCM).....	20.04	11.30	10.14
(PPM-WET).....	16.78	9.40	8.45
(PPM-DRY).....	17.20	9.70	8.70
(PPM-DRY @ 7% O2).....	481.60	271.60	243.60
CO emission rate.....(LB/HR)	5.133	2.790	2.510

CO = Carbon monoxide

A trailing '<' symbol indicates that the true value
is less than or equal to the reported value

Test No. 5
Line 1 Konus Stack

Results of CO Determinations -----Method 10

	Run 1	Run 2	Run 3
Date of run	06-08-94	06-08-94	06-08-94
Time run start/end.....(HRS)	1538/1640	1708/1811	1835/1938
Total sampling time....(MIN)	60.0	60.0	60.0
Moisture content.....(%V/V)	9.70	8.55	10.88
O2 Concentration.....(%V/V)	14.50	15.50	13.50
Volumetric flow rate (DSCFM)	10771	11266	10936
CO concentration.....			
(GR/DSCF).....	0.0468	0.0458	0.3582
(MG/DSCM).....	107.18	104.85	820.16
(PPM-WET).....	83.08	82.31	627.40
(PPM-DRY).....	92.00	90.00	704.00
(PPM-DRY @ 7% O2).....	198.15	229.09	1314.
CO emission rate.....(LB/HR)	4.322	4.422	33.578

CO = Carbon monoxide

A trailing '<' symbol indicates that the true value
is less than or equal to the reported value

Test No. 6
Line 1 Konus Stack

Results of CO Determinations -----Method 10

	Run 1	Run 2	Run 3
Date of run	06-09-94	06-09-94	06-09-94
Time run start/end.....(HRS)	1345/1606	1632/1743	1802/1904
Total sampling time....(MIN)	60.0	60.0	60.0
Moisture content.....(%V/V)	7.68	9.37	8.54
O2 Concentration.....(%V/V)	14.50	13.50	14.20
Volumetric flow rate (DSCFM)	10945	10781	10817
CO concentration.....			
(GR/DSCF).....	0.0312	0.0909	0.0271
(MG/DSCM).....	71.53	208.19	62.09
(PPM-WET).....	56.68	161.96	48.75
(PPM-DRY).....	61.40	178.70	53.30
(PPM-DRY @ 7% O2).....	132.25	333.57	109.74
CO emission rate.....(LB/HR)	2.931	8.402	2.515

CO = Carbon monoxide

A trailing '<' symbol indicates that the true value
is less than or equal to the reported value

Test No. 8
Line 1 Konus Stack

Results of CO Determinations -----Method 10

	Run 1	Run 2	Run 3
Date of run	06-09-94	06-09-94	06-09-94
Time run start/end.....(HRS)	0851/1052	1240/1534	1610/1812
Total sampling time....(MIN)	120.0	120.0	120.0
Moisture content.....(%V/V)	8.07	8.52	9.91
O2 Concentration.....(%V/V)	15.40	14.90	13.80
Volumetric flow rate (DSCFM)	10888	10670	10885
CO concentration.....-			
(GR/DSCF).....	0.0532	0.0530	0.0688
(MG/DSCM).....	121.74	121.28	157.62
(PPM-WET).....	96.07	95.23	121.89
(PPM-DRY).....	104.50	104.10	135.30
(PPM-DRY @ 7% O2).....	261.25	238.92	263.08
CO emission rate.....(LB/HR)	4.962	4.844	6.423

CO = Carbon monoxide

A trailing '<' symbol indicates that the true value
is less than or equal to the reported value

Test No. 16
Line 2 Konus Stack

Results of CO Determinations -----Method 10

	Run 1	Run 2	Run 3
Date of run	06-08-94	06-08-94	06-08-94
Time run start/end.....(HRS)	0757/0858	0920/1021	1114/1215
Total sampling time....(MIN)	60.0	60.0	60.0
Moisture content.....(%V/V)	6.60	6.99	7.80
O2 Concentration.....(%V/V)	16.40	16.50	15.90
Volumetric flow rate (DSCFM)	16583	16372	15772
CO concentration.....			
(GR/DSCF).....	0.0371	0.0341	0.0315
(MG/DSCM).....	85.05	78.06	72.23
(PPM-WET).....	68.18	62.32	57.16
(PPM-DRY).....	73.00	67.00	62.00
(PPM-DRY @ 7% O2).....	222.17	208.44	170.20
CO emission rate.....(LB/HR)	5.280	4.784	4.265

CO = Carbon monoxide

A trailing '<' symbol indicates that the true value
is less than or equal to the reported value

Test No. 14
Line 2 Press RTO Outlet Stack

Results of CO Determinations -----Method 10

	Run 1	Run 2	Run 3
Date of run	06-09-94	06-09-94	06-09-94
Time run start/end.....(HRS)	1240/1342	1425/1527	1605/1719
Total sampling time....(MIN)	60.0	60.0	60.0
Moisture content.....(%V/V)	2.35	2.55	2.05
O2 Concentration.....(%V/V)	20.60	20.60	20.55
Volumetric flow rate (DSCFM)	81742	80986	79766
CO concentration.....			
(GR/DSCF).....	0.0046	0.0064	0.0059
(MG/DSCM).....	10.48	14.68	13.40
(PPM-WET).....	8.79	12.28	11.26
(PPM-DRY).....	9.00	12.60	11.50
(PPM-DRY @ 7% O2).....	315.00	441.00	357.78
CO emission rate.....(LB/HR)	3.209	4.450	4.001

CO = Carbon monoxide

A trailing '<' symbol indicates that the true value
is less than or equal to the reported value

3.6 Results of Formaldehyde Determinations

Test No. 1
Line 1 Press RTO Outlet Stack

Results of Formaldehyde Tests ----- EPA Method 0011

	Run 1 06-07-94	Run 2 06-07-94	Run 3 06-07-94
Date of run			
Time run start/end.....(HRS)	1250/1352	1420/1522	1545/1646
Static pressure.....(IN.WC)	-0.30	-0.30	-0.30
Cross sectional area (SQ.FT)	31.09	31.09	31.09
Pitot tube coefficient.....	.840	.840	.840
Water in sample gas			
condenser.....(ML)	0.0	0.0	0.0
impingers.....(GRAMS)	5.0	10.0	17.0
desiccant.....(GRAMS)	20.0	14.0	17.0
total.....(GRAMS)	25.0	24.0	34.0
Formaldehyde in sample..(uG)	430	14	610
Gas meter coefficient.....	1.0066	1.0066	1.0066
Barometric pressure..(IN.HG)	28.73	28.73	28.73
Avg. orif.pres.drop..(IN.WC)	2.58	2.68	2.73
Avg. gas meter temp..(DEF-F)	84.2	86.5	86.8
Volume through gas meter....			
at meter conditions...(CF)	54.39	55.52	56.16
standard conditions.(DSCF)	51.32	52.18	52.76
Total sampling time....(MIN)	60.00	60.00	60.00
Nozzle diameter.....(IN)	.270	.270	.270
Avg.stack gas temp ..(DEG-F)	252	251	252
Volumetric flow rate.....			
actual.....(ACFM)	97234	97872	99119
dry standard.....(DSCFM)	67660	68218	68471
Isokinetic variation.....(%)	98.9	99.7	100.5
CH2O concentration.....			
(MG/DSCM).....	0.30	0.01	0.41
(PPM-DRY).....	0.24	0.01	0.33
(PPM-WET).....	0.23	0.01	0.32
CH2O emission rate...(LB/HR)	0.07544	0.00244	0.10539

CH2O = Formaldehyde

A trailing '<' symbol indicates that the true value is less than or equal to the reported value

Test No. 6
Line 1 Konus Stack

Results of Formaldehyde Tests ----- EPA Method 0011

	Run 1 06-09-94	Run 2 06-09-94	Run 3 06-09-94
Date of run			
Time run start/end.....(HRS)	1345/1606	1632/1743	1802/1904
Static pressure.....(IN.WC)	-0.20	-0.20	-0.20
Cross sectional area (SQ.FT)	14.75	14.75	14.75
Pitot tube coefficient.....	.840	.840	.840
Water in sample gas			
condenser.....(ML)	0.0	0.0	0.0
impingers.....(GRAMS)	68.0	94.0	79.0
desiccant.....(GRAMS)	16.0	11.0	15.0
total.....(GRAMS)	84.0	105.0	94.0
Formaldehyde in sample..(uG)	56	140	79
Gas meter coefficient.....	0.9974	0.9974	0.9974
Barometric pressure..(IN.HG)	28.90	28.90	28.90
Avg. orif.pres.drop..(IN.WC)	2.12	2.14	2.14
Avg. gas meter temp..(DEF-F)	84.3	89.0	89.0
Volume through gas meter....			
at meter conditions...(CF)	50.66	51.40	50.95
standard conditions.(DSCF)	47.58	47.86	47.45
Total sampling time....(MIN)	60.00	60.00	60.00
Nozzle diameter.....(IN)	.445	.445	.445
Avg.stack gas temp ..(DEG-F)	329	329	327
Volumetric flow rate.....			
actual.....(ACFM)	18340	18419	18268
dry standard.....(DSCFM)	10945	10781	10817
Isokinetic variation.....(%)	99.0	101.1	99.9
CH2O concentration.....			
(MG/DSCM).....	0.04	0.10	0.06
(PPM-DRY).....	0.03	0.08	0.05
(PPM-WET).....	0.03	0.08	0.04
CH2O emission rate...(LB/HR)	0.00171	0.00419	0.00239

CH2O = Formaldehyde

A trailing '<' symbol indicates that the true value
is less than or equal to the reported value

Test No. 12
Line 2 Press RTO Outlet Stack

Results of Formaldehyde Tests ----- EPA Method 0011

	Run 1 06-10-94	Run 2 06-10-94	Run 3 06-10-94
Date of run			
Time run start/end.....(HRS)	815/ 918	941/1043	1121/1333
Static pressure.....(IN.WC)	-0.98	-0.98	-0.98
Cross sectional area (SQ.FT)	31.71	31.71	31.71
Pitot tube coefficient.....	.840	.840	.840
Water in sample gas			
condenser.....(ML)	0.0	0.0	0.0
impingers.....(GRAMS)	14.0	14.0	10.0
desiccant.....(GRAMS)	13.0	12.0	9.0
total.....(GRAMS)	27.0	26.0	19.0
Formaldehyde in sample..(uG)	400	340	360
Gas meter coefficient.....	0.9947	0.9947	0.9947
Barometric pressure..(IN.HG)	28.93	28.93	28.93
Avg. orif.pres.drop..(IN.WC)	2.32	2.37	2.35
Avg. gas meter temp..(DEG-F)	82.1	93.8	99.9
Volume through gas meter....			
at meter conditions...(CF)	50.53	51.53	51.63
standard conditions.(DSCF)	47.60	47.52	47.09
Total sampling time....(MIN)	60.00	60.00	60.00
Nozzle diameter.....(IN)	.240	.240	.240
Avg.stack gas temp ..(DEG-F)	251	255	255
Volumetric flow rate.....			
actual.....(ACFM)	114407	114678	113731
dry standard.....(DSCFM)	79772	79658	79469
Isokinetic variation.....(%)	100.4	100.4	99.7
CH2O concentration.....			
(MG/DSCM).....	0.30	0.25	0.27
(PPM-DRY).....	0.24	0.20	0.22
(PPM-WET).....	0.23	0.20	0.21
CH2O emission rate...(LB/HR)	0.08915	0.07581	0.08080

CH2O = Formaldehyde

A trailing '<' symbol indicates that the true value is less than or equal to the reported value

Test No. 17
Line 2 Konus Stack

Results of Formaldehyde Tests ----- EPA Method 0011

	Run 1	Run 2	Run 3
Date of run	06-08-94	06-08-94	06-08-94
Time run start/end.....(HRS)	1446/1553	1616/1718	1742/1843
Static pressure.....(IN.WC)	-0.28	-0.28	-0.28
Cross sectional area (SQ.FT)	14.47	14.47	14.47
Pitot tube coefficient.....	.840	.840	.840
Water in sample gas			
condenser.....(ML)	0.0	0.0	0.0
impingers.....(GRAMS)	54.0	52.0	59.0
desiccant.....(GRAMS)	17.0	17.0	17.0
total.....(GRAMS)	71.0	69.0	76.0
Formaldehyde in sample..(uG)	94	66	140
Gas meter coefficient.....	0.9961	0.9961	0.9961
Barometric pressure..(IN.HG)	28.98	28.98	28.98
Avg. orif.pres.drop..(IN.WC)	2.32	2.28	2.79
Avg. gas meter temp..(DEF-F)	88.1	93.9	93.4
Volume through gas meter....			
at meter conditions...(CF)	52.98	52.93	58.34
standard conditions.(DSCF)	49.51	48.94	54.06
Total sampling time....(MIN)	60.00	60.00	60.00
Nozzle diameter.....(IN)	.368	.368	.368
Avg.stack gas temp ..(DEG-F)	326	324	321
Volumetric flow rate.....			
actual.....(ACFM)	26905	26135	28737
dry standard.....(DSCFM)	16380	15973	17642
Isokinetic variation.....(%)	98.7	100.1	100.1
CH2O concentration.....			
(MG/DSCM).....	0.07	0.05	0.09
(PPM-DRY).....	0.05	0.04	0.07
(PPM-WET).....	0.05	0.04	0.07
CH2O emission rate...(LB/HR)	0.00414	0.00286	0.00608

CH2O = Formaldehyde

A trailing '<' symbol indicates that the true value is less than or equal to the reported value

3.7 Results of MDI Determinations

Test No. 2
Line 1 Press RTO Outlet Stack

Results of MDI Determinations.....

	Run 1	Run 2	Run 3
Date of run	06-08-94	06-08-94	06-08-94
Time run start/end.....(HRS)	815/ 916	945/1046	1115/1216
Static pressure.....(IN.WC)	-0.35	-0.35	-0.35
Cross sectional area (SQ.FT)	31.09	31.09	31.09
Pitot tube coefficient.....	.840	.840	.840
Water in sample gas			
condenser.....(ML)	0.0	0.0	0.0
impingers.....(GRAMS)	16.0	17.0	13.0
desiccant.....(GRAMS)	10.0	10.0	10.0
total.....(GRAMS)	26.0	27.0	23.0
MDI in Sample.....(ug)	5.2	<2.5	5.4
Gas meter coefficient.....	1.0066	1.0066	1.0066
Barometric pressure..(IN.HG)	28.98	28.98	28.98
Avg. orif.pres.drop..(IN.WC)	1.24	1.28	1.31
Avg. gas meter temp..(DEF-F)	59.5	72.1	75.2
Volume through gas meter....			
at meter conditions...(CF)	36.68	37.74	38.41
standard conditions.(DSCF)	36.45	36.62	37.05
Total sampling time....(MIN)	60.00	60.00	60.00
Nozzle diameter.....(IN)	.225	.225	.225
Avg.stack gas temp ..(DEG-F)	248	251	253
Volumetric flow rate.....			9906.2
actual.....(ACFM)	98092	98949	100145
dry standard.....(DSCFM)	68445	68682	69702
Isokinetic variation.....(%)	100.0	100.1	68943 99.8
MDI Concentration			
.....(mg/Nm ³)	0.00504	< 0.00241	0.00515
.....(ppm)	0.000484	< 0.000232	0.000495
MDI Emission Rate			
.....(LB/HR)	0.001292	< 0.00062	0.001344

Test No. 13
Line 2 Press RTO Outlet Stack

Results of MDI Determinations.....

	Run 1	Run 2	Run 3
Date of run	06-09-94	06-09-94	06-09-94
Time run start/end.....(HRS)	1325/1440	1518/1641	1712/1828
Static pressure.....(IN.WC)	-0.98	-0.98	-0.98
Cross sectional area (SQ.FT)	31.71	31.71	31.71
Pitot tube coefficient.....	.840	.840	.840
Water in sample gas			
condenser.....(ML)	0.0	0.0	0.0
impingers.....(GRAMS)	0.0	0.0	0.0
desiccant.....(GRAMS)	29.0	19.0	16.0
total.....(GRAMS)	29.0	19.0	16.0
MDI in Sample.....(ug)	12.2	< 2.5	6.5
Gas meter coefficient.....	0.9983	0.9983	0.9983
Barometric pressure..(IN.HG)	28.90	28.90	28.90
Avg. orif.pres.drop..(IN.WC)	2.14	0.79	0.87
Avg. gas meter temp..(DEF-F)	87.3	93.7	95.3
Volume through gas meter....			
at meter conditions...(CF)	60.73	37.29	39.32
standard conditions.(DSCF)	56.78	34.34	36.12
Total sampling time....(MIN)	72.00	72.00	72.00
Nozzle diameter.....(IN)	.240	.189	.189
Avg.stack gas temp ..(DEG-F)	256	259	257
Volumetric flow rate.....			
actual.....(ACFM)	115175	112761	118035
dry standard.....(DSCFM)	79909	77756	81992
Isokinetic variation.....(%)	99.7	99.9	99.6
MDI Concentration			
.....(mg/Nm ³)	0.00759	< 0.00257	0.00635
.....(ppm)	0.000729	< 0.000247	0.000611
MDI Emission Rate			
.....(LB/HR)	0.00227	< 0.00075	0.00195

3.8 Results of Phenol Determinations

Test No. 7
Line 1 Konus Stack

Results of Phenol Determinations -----

	Run 1	Run 2	Run 3
Date of run	06-09-94	06-09-94	06-09-94
Time run start/end.....(HRS)	0845/0945	1000/1100	1111/1320
Barometric pressure..(IN.HG)	28.90	28.90	28.90
Meter temperature....(DEG-F)	72.30	76.90	79.10
Meter correction coefficient	0.9974	0.9974	0.9974
Volume through gas meter....			
at meter conditions...(CF)	45.200	45.630	45.500
standard conditions (DSCF)	43.388	43.426	43.125
Total sampling time....(MIN)	60.0	60.0	60.0
Moisture content.....(%V/V)	6.69	7.24	7.85
Volumetric flow rate (DSCFM)	10888	10670	10885
Phenol in sample.....(uG)	840.00<	840.00<	840.00<
Phenol concentration.....			
(GR/10 ³ DSCF).....	0.2987<	0.2985<	0.3005<
(uG/DSCM).....	684.19<	683.60<	688.36<
(PPB-DRY).....	174.84<	174.69<	175.90<
(PPB-WET).....	163.14<	162.04<	162.10<
Phenol emis. rate(10 ⁻³ LB/HR)	27.877<	27.296<	28.040<

A trailing '<' symbol indicates that the true value
is less than or equal to the reported value

Analysis performed according to NIOSH Method 3502

Test No. 18
Line 2 Konus Stack

Results of Phenol Determinations -----

	Run 1	Run 2	Run 3
Date of run	06-08-94	06-08-94	06-08-94
Time run start/end.....(HRS)	1447/1554	1616/1718	1743/1844
Barometric pressure...(IN.HG)	28.98	28.98	28.98
Meter temperature....(DEG-F)	81.29	86.33	87.38
Meter correction coefficient	0.9930	0.9930	0.9930
Volume through gas meter....			
at meter conditions...(CF)	45.700	45.960	46.350
standard conditions (DSCF)	43.068	42.913	43.194
Total sampling time.....(MIN)	60.0	60.0	60.0
Moisture content.....(%V/V)	6.33	6.23	6.22
Volumetric flow rate (DSCFM)	16380	15973	17642
Phenol in sample.....(uG)	840.00<	840.00<	840.00<
Phenol concentration.....			
(GR/10 ³ DSCF).....	0.3010<	0.3020<	0.3001<
(uG/DSCM).....	689.28<	691.76<	687.26<
(PPB-DRY).....	176.14<	176.77<	175.62<
(PPB-WET).....	164.99<	165.76<	164.70<
Phenol emis. rate(10 ⁻³ LB/HR)	42.251<	41.350<	45.373<

A trailing '<' symbol indicates that the true value
is less than or equal to the reported value

Analysis performed according to NIOSH Method 3502

3.9 PAH Sampling Data

Test No. 8
Line 1 Konus Stack

Sampling Data for PAH Determinations-----SW846 Method 0010

	Run 1	Run 2	Run 3
Date of run	06-09-94	06-09-94	06-09-94
Time run start/end.....(HRS)	851/1052	1240/1534	1610/1812
Static pressure.....(IN.WC)	-0.20	-0.20	-0.20
Cross sectional area (SQ.FT)	14.75	14.75	14.75
Pitot tube coefficient.....	0.840	0.840	0.840
Water in sample gas			
condenser.....(ML)	133.0	139.0	160.0
impingers.....(GRAMS)	0.0	0.0	0.0
desiccant.....(GRAMS)	26.0	30.0	44.0
total.....(GRAMS)	159.0	169.0	204.0
Gas meter coefficient.....	0.9961	0.9961	0.9961
Barometric pressure..(IN.HG)	28.90	28.90	28.90
Avg. orif.pres.drop..(IN.WC)	1.70	1.71	1.84
Avg. gas meter temp..(DEG-F)	78.2	84.8	92.7
Volume through gas meter....			
at meter conditions...(CF)	89.94	91.32	94.60
standard conditions.(DSCF)	85.23	85.49	87.32
standard conditions..(NM ³)	2.413	2.421	2.473
Total sampling time....(MIN)	120.00	120.00	120.00
Nozzle diameter.....(IN)	.422	.422	.422
Avg.stack gas temp ..(DEG-F)	332	327	329
Volumetric flow rate.....			
actual.....(ACFM)	18391	18003	18707
dry standard.....(DSCFM)	10888	10670	10885
Isokinetic variation.....(%)	99.1	101.4	101.6

Test No. 19
Line 2 Konus Stack

Sampling Data for PAH Determinations-----SW846 Method 0010

	Run 1	Run 2	Run 3
Date of run	06-07-94	06-07-94	06-07-94
Time run start/end.....(HRS)	827/1032	1136/1342	1425/1627
Static pressure.....(IN.WC)	-0.26	-0.26	-0.26
Cross sectional area (SQ.FT)	14.47	14.47	14.47
Pitot tube coefficient.....	0.840	0.840	0.840
Water in sample gas			
condenser.....(ML)	172.0	158.0	137.0
impingers.....(GRAMS)	0.0	0.0	0.0
desiccant.....(GRAMS)	33.0	37.0	61.0
total.....(GRAMS)	205.0	195.0	198.0
Gas meter coefficient.....	0.9961	0.9961	0.9961
Barometric pressure..(IN.HG)	28.73	28.73	28.73
Avg. orif.pres.drop..(IN.WC)	2.64	2.71	2.80
Avg. gas meter temp..(DEF-F)	77.1	86.1	89.3
Volume through gas meter....			
at meter conditions...(CF)	112.39	114.57	117.00
standard conditions.(DSCF)	106.35	106.64	108.30
standard conditions..(NM ³)	3.011	3.020	3.067
Total sampling time....(MIN)	120.00	120.00	120.00
Nozzle diameter.....(IN)	.364	.364	.364
Avg.stack gas temp ..(DEG-F)	333	338	332
Volumetric flow rate.....			
actual.....(ACFM)	30553	30649	30805
dry standard.....(DSCFM)	17895	17923	18140
Isokinetic variation.....(%)	99.2	99.3	99.6

4 RESULTS OF FUEL ANALYSIS

INTERPOLL LABORATORIES, INC.

Fuel Laboratory
(612) 786-6020

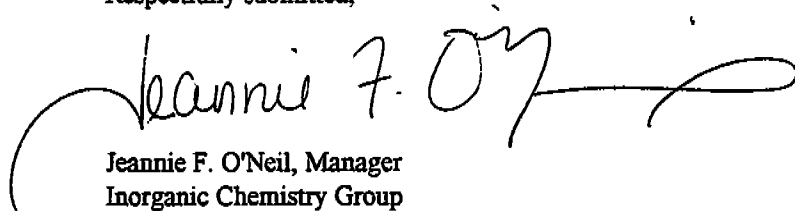
6/22/94

Client: LOUISIANA PACIFIC, HAYWARD
Laboratory Log Number: 3097-185-7743
Sample Identification: WOOD BARK 6/10/94

Ultimate Analysis WT %

Parameter	Moisture & Ash Free	Moisture Free	As Received
Moisture, Total			39.47
Ash		3.08	1.86
Carbon	51.83	50.23	30.41
Hydrogen	5.63	5.46	3.30
Nitrogen	0.28	0.27	0.16
Oxygen (calculated)	42.19	40.89	24.75
Sulfur	0.07	0.07	0.07
Heating Value, BTU/LB	9187	8904	5390

Respectfully submitted,



Jeannie F. O'Neil, Manager
Inorganic Chemistry Group

8761

APPENDIX A

VOLUMETRIC FLOW RATE DETERMINATIONS

APPENDIX A

VOLUMETRIC FLOW RATE DETERMINATIONS

Test No. 3
Line 1 Press RTO Outlet Stack

Results of Volumetric Flow Rate Determination-----Method 2

Date of Determination.....	06-10-94
Time of Determination.....(HRS)	837
Barometric pressure.....(IN.HG)	28.93
Pitot tube coefficient.....	.84
Number of sampling ports.....	2
Total number of points.....	20
Shape of duct.....	Round
Stack diameter.....(IN)	75.5
Duct area.....(SQ.FT)	31.09
Direction of flow.....	UP
Static pressure.....(IN.WC)	-.43
Avg. gas temp.....(DEG-F)	252
Moisture content.....(% V/V)	2.45
Avg. linear velocity.....(FT/SEC)	51.8
Gas density.....(LB/ACF)	.05326
Molecular weight.....(LB/LBMOLE)	28.88
Mass flow of gas.....(LB/HR)	309057
Volumetric flow rate.....	
actual.....(ACFM)	96716
dry standard.....(DSCFM)	67613

Test No. 5
Line 1 Press RTO Inlet

Results of Volumetric Flow Rate Determination-----Method 2

Date of Determination.....	06-10-94
Time of Determination.....(HRS)	841
Barometric pressure.....(IN.HG)	28.93
Pitot tube coefficient.....	.84
Number of sampling ports.....	2
Total number of points.....	24
Shape of duct.....	Round
Stack diameter.....(IN)	53.125
Duct area.....(SQ.FT)	15.39
Direction of flow.....	DOWN
Static pressure.....(IN.WC)	-2.95
Avg. gas temp.....(DEG-F)	116
Moisture content.....(% V/V)	1.92
Avg. linear velocity.....(FT/SEC)	72.0
Gas density.....(LB/ACF)	.06541
Molecular weight.....(LB/LBMOLE)	28.84
Mass flow of gas.....(LB/HR)	260943
Volumetric flow rate.....	
actual.....(ACFM)	66488
dry standard.....(DSCFM)	57368

Test No. 5
Line 1 Konus Stack

Results of Volumetric Flow Rate Determination-----Method 2

Date of Determination.....	06-08-94
Time of Determination.....(HRS)	800
Barometric pressure.....(IN.HG)	28.98
Pitot tube coefficient.....	.84
Number of sampling ports.....	2
Total number of points.....	20
Shape of duct.....	Round
Stack diameter.....(IN)	52
Duct area.....(SQ.FT)	14.75
Direction of flow.....	UP
Static pressure.....(IN.WC)	-.2
Avg. gas temp.....(DEG-F)	326
Moisture content.....(% V/V)	9.70
Avg. linear velocity.....(FT/SEC)	24.0
Gas density.....(LB/ACF)	.04800
Molecular weight.....(LB/LBMOLE)	29.54
Mass flow of gas.....(LB/HR)	61145
Volumetric flow rate.....	
actual.....(ACFM)	21232
dry standard.....(DSCFM)	12469

Test No. 8
Line 1 Konus Stack

Results of Volumetric Flow Rate Determination-----Method 2

Date of Determination.....	06-09-94
Time of Determination.....(HRS)	830
Barometric pressure.....(IN.HG)	28.9
Pitot tube coefficient.....	.84
Number of sampling ports.....	2
Total number of points.....	24
Shape of duct.....	Round
Stack diameter.....(IN)	52
Duct area.....(SQ.FT)	14.75
Direction of flow.....	UP
Static pressure.....(IN.WC)	-.2
Avg. gas temp.....(DEG-F)	330
Moisture content.....(% V/V)	10.29
Avg. linear velocity.....(FT/SEC)	21.2
Gas density.....(LB/ACF)	.04739
Molecular weight.....(LB/LBMOLE)	29.46
Mass flow of gas.....(LB/HR)	53323
Volumetric flow rate.....	
actual.....(ACFM)	18752
dry standard.....(DSCFM)	10854

Test No. 19
Line 2 Konus Stack

Results of Volumetric Flow Rate Determination-----Method 2

Date of Determination.....	06-07-94
Time of Determination.....(HRS)	800
Barometric pressure.....(IN.HG)	28.73
Pitot tube coefficient.....	.84
Number of sampling ports.....	2
Total number of points.....	24
Shape of duct.....	Round
Stack diameter.....(IN)	51.5
Duct area.....(SQ.FT)	14.47
Direction of flow.....	UP
Static pressure.....(IN.WC)	-.26
Avg. gas temp.....(DEG-F)	328
Moisture content.....(% V/V)	8.52
Avg. linear velocity.....(FT/SEC)	35.1
Gas density.....(LB/ACF)	.04950
Molecular weight.....(LB/LBMOLE)	30.73
Mass flow of gas.....(LB/HR)	90370
Volumetric flow rate.....	
actual.....(ACFM)	30430
dry standard.....(DSCFM)	17898

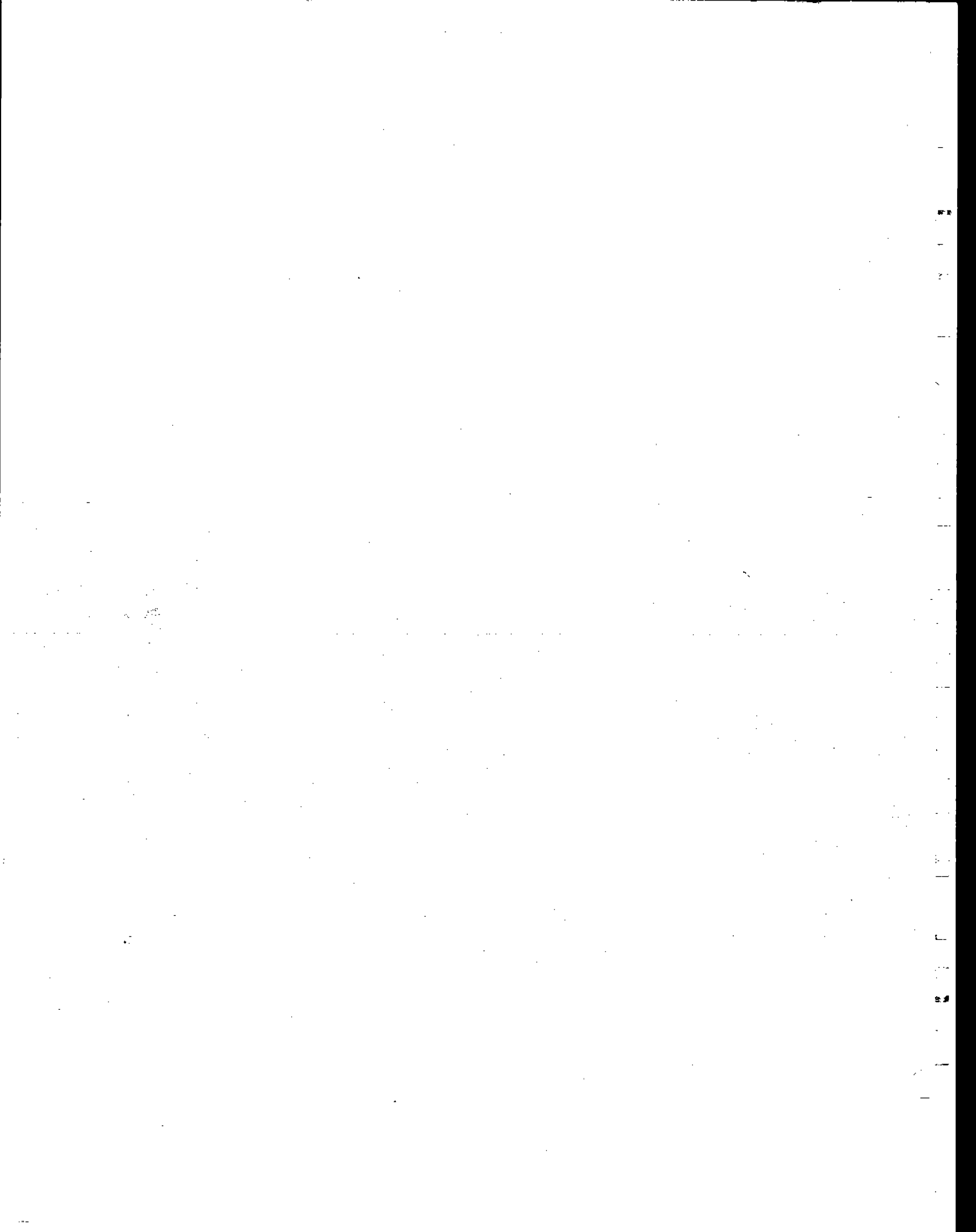
Test No. 21
Line 2 Press RTO Inlet

Results of Volumetric Flow Rate Determination-----Method 2

Date of Determination.....	06-09-94
Time of Determination.....(HRS)	1400
Barometric pressure.....(IN.HG)	28.9
Pitot tube coefficient.....	.84
Number of sampling ports.....	2
Total number of points.....	12
Shape of duct.....	Round
Stack diameter.....(IN)	58.5
Duct area.....(SQ.FT)	18.67
Direction of flow.....	HORIZONTAL
Static pressure.....(IN.WC)	-4.4
Avg. gas temp.....(DEG-F)	116
Moisture content.....(% V/V)	2.46
Avg. linear velocity.....(FT/SEC)	81.3
Gas density.....(LB/ACF)	.06493
Molecular weight.....(LB/LBMOLE)	28.84
Mass flow of gas.....(LB/HR)	354569
Volumetric flow rate.....	
actual.....(ACFM)	91017
dry standard.....(DSCFM)	77678

APPENDIX B

LOCATION OF TEST PORTS



Hayward test protocol

LINE 2 DRYER RTO

LINE 2 DRYERS
LOCATION

LINE 1 DRYERS
LOCATION

LINE 1 DRYER RTO

LINE 2 PRESS RTO

LINE 2 PRESS
LOCATION

LINE 1 PRESS
LOCATION

LINE 1 PRESS RTO

THERMAL OIL HEATERS
LOCATION

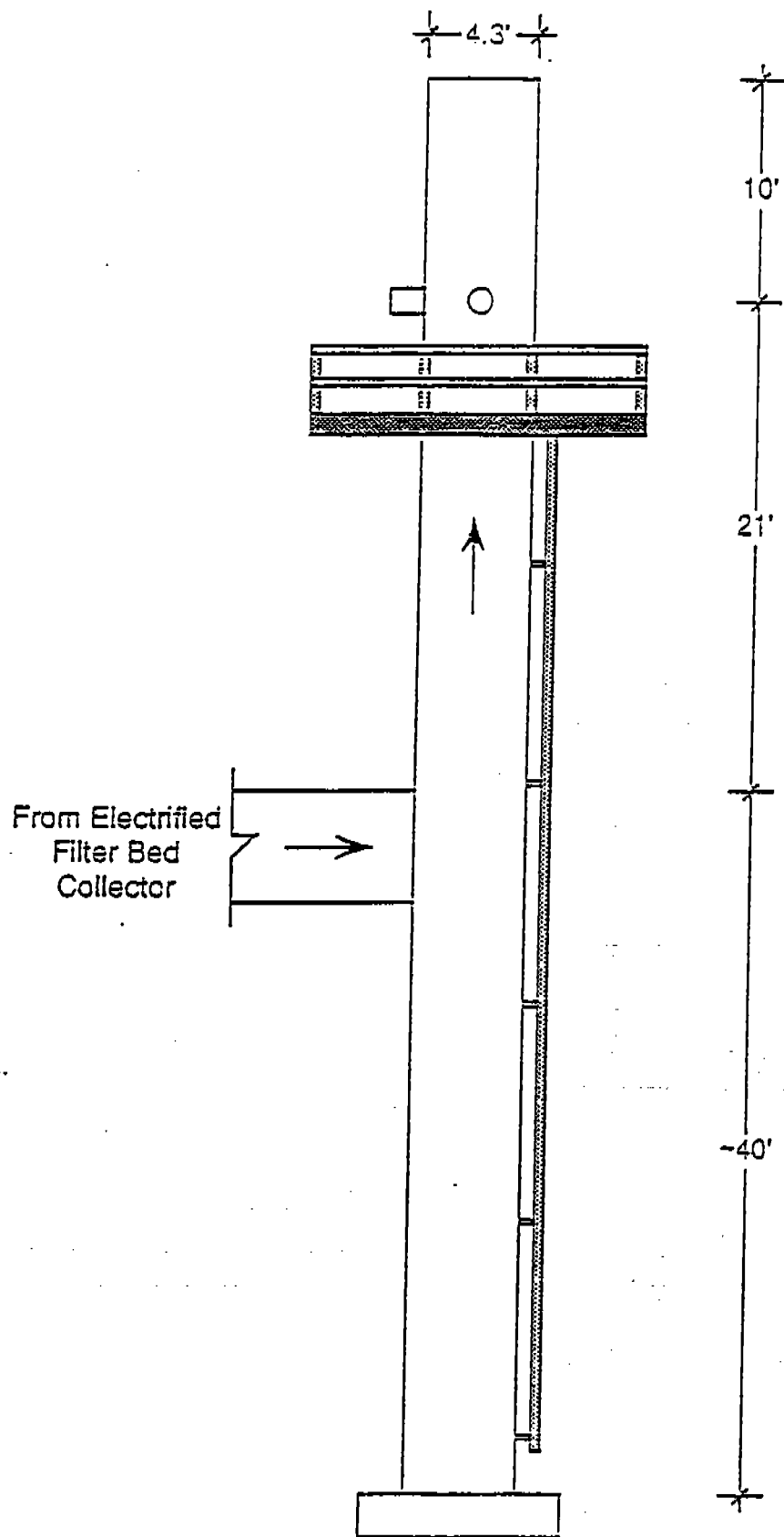
LOG YARD

LOG YARD

SCALES

HAYWARD, WI
DRAWING 1
RTO GENERAL
PLANT ARRANGEMENT

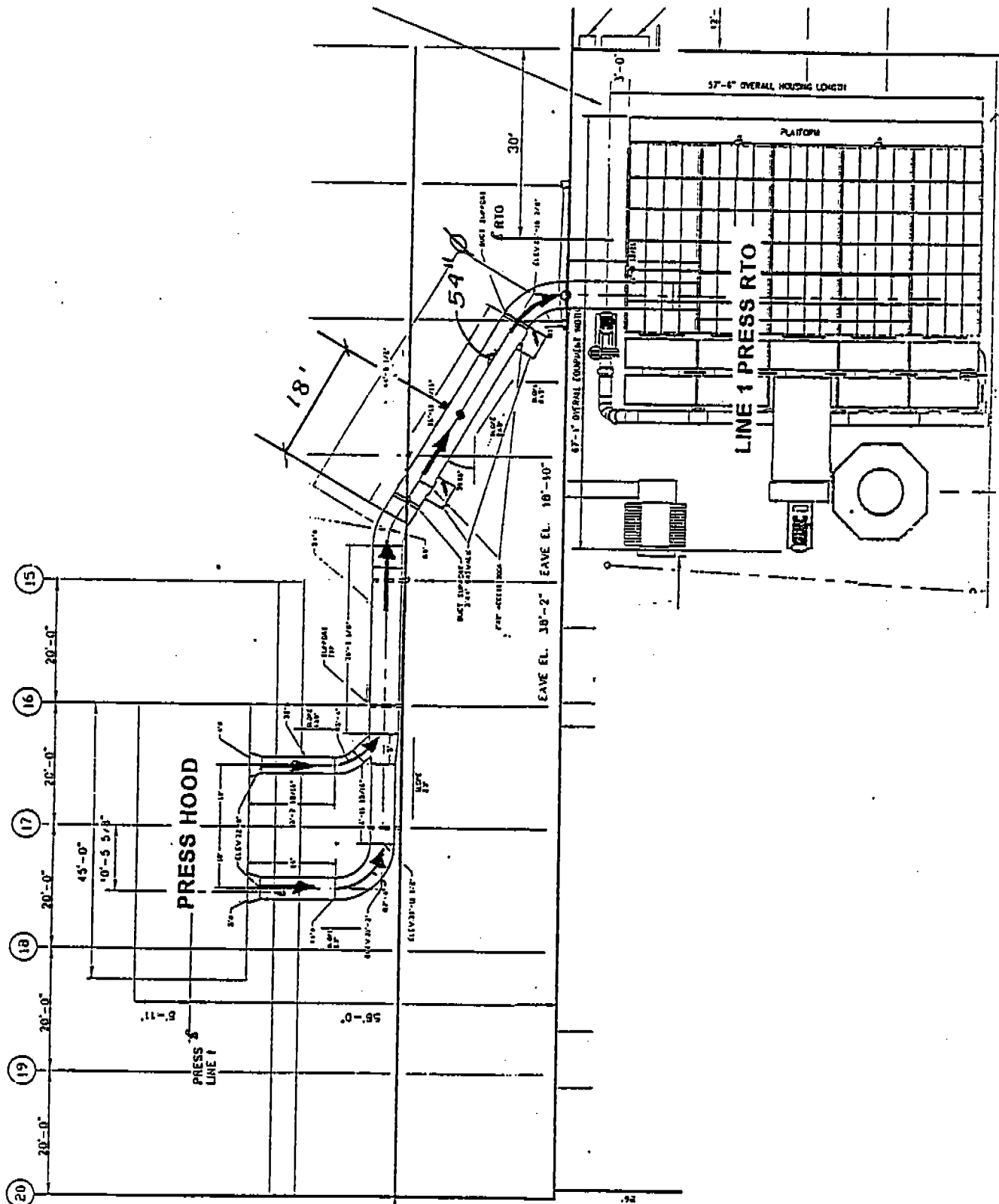
B-1



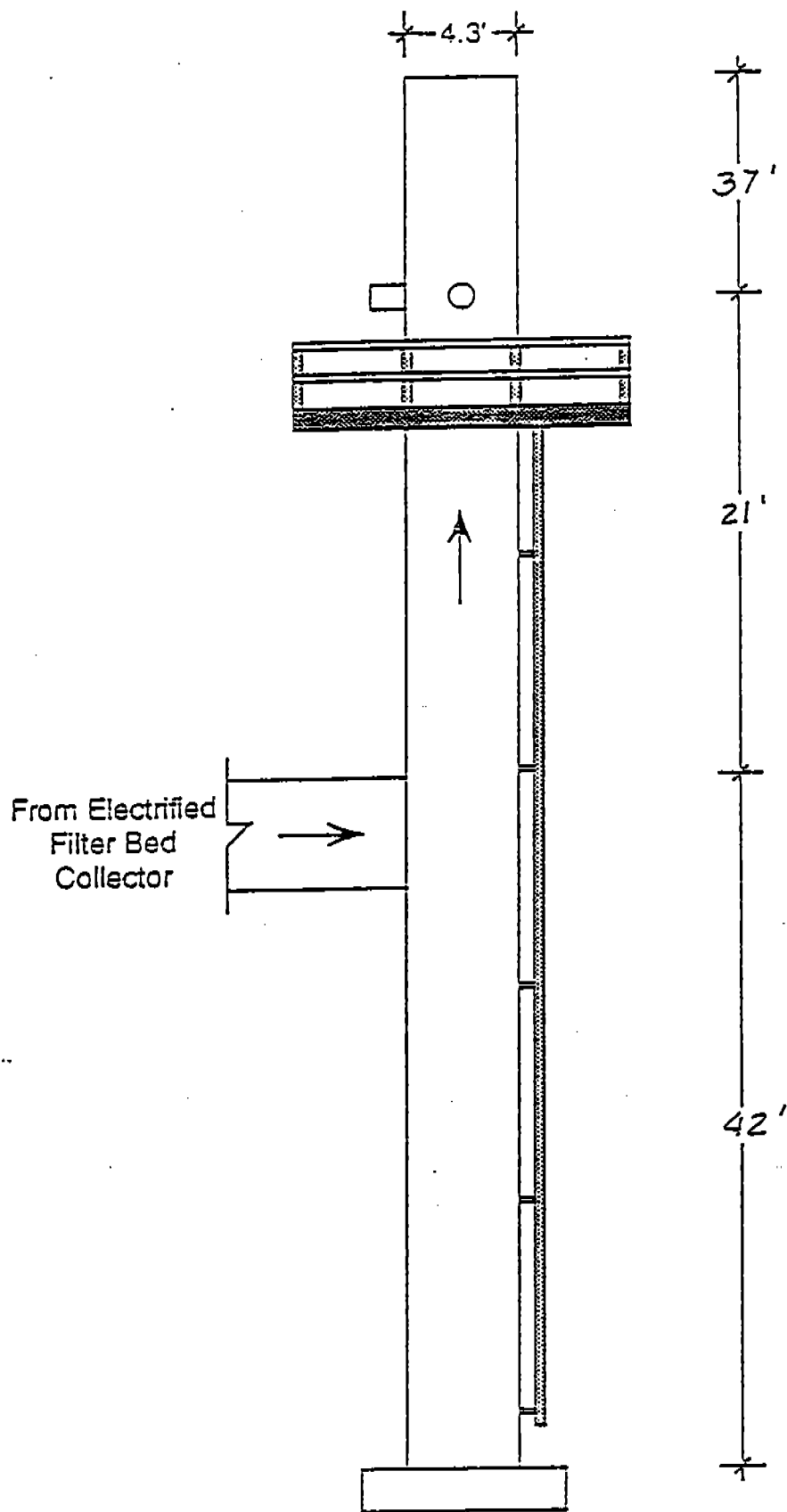
HAYWARD, WI
DRAWING 10
LINE 1
THERMAL OIL HEATER
STACK
ELEVATION

Hayward test protocol

HAYWARD, WI
DRAWING 7
PRESS RTO STACK
TYPICAL FOR BOTH LINES
ELEVATION



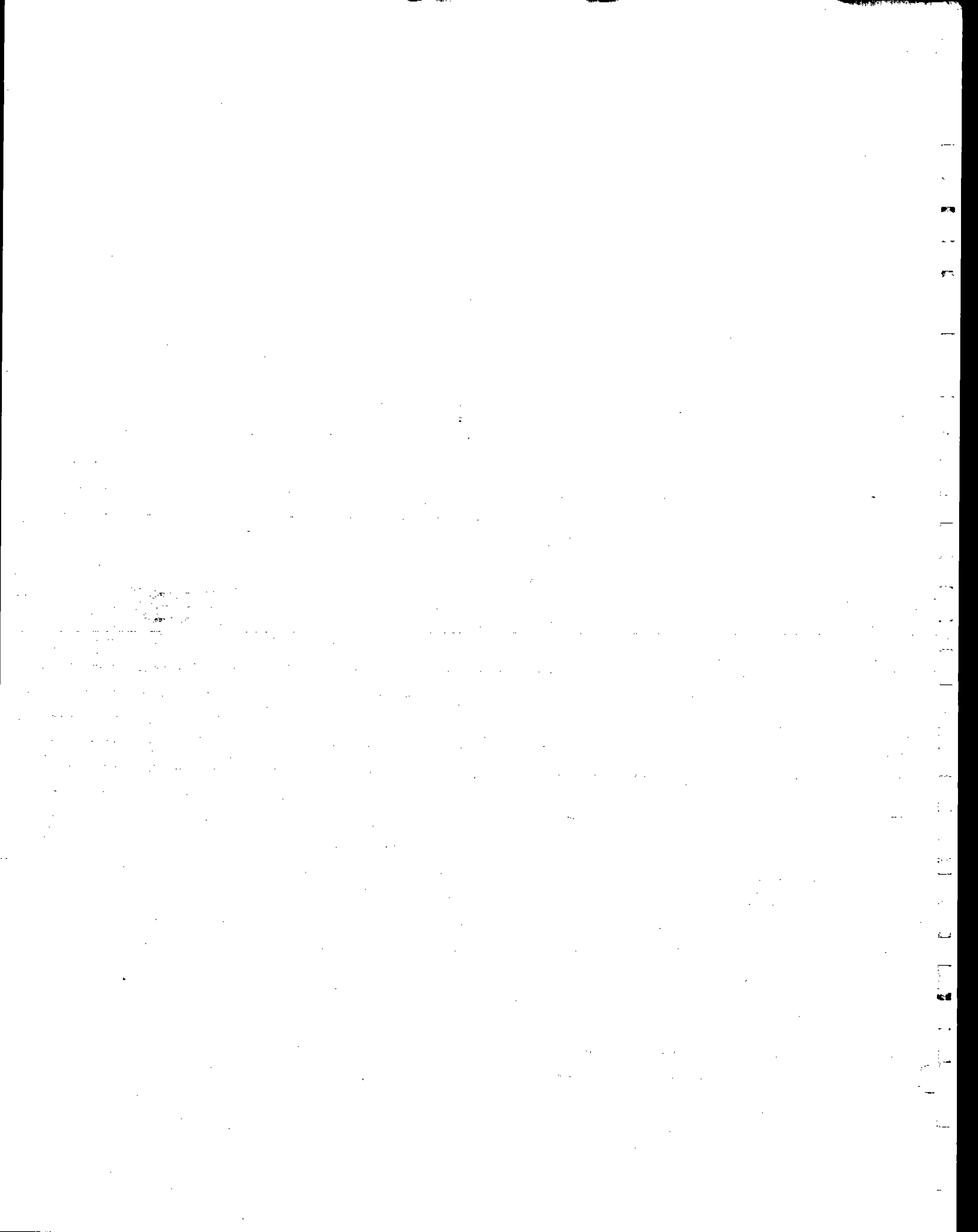
HAYWARD, WI
DRAWING 8
GAS FLOW FROM
LINE 1 PRESS
TO RTO
PLAN



HAYWARD, WI
DRAWING 11
LINE 2
THERMAL OIL HEATER
STACK
ELEVATION

APPENDIX C

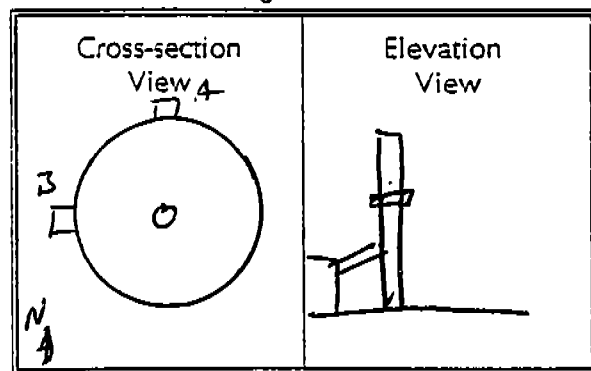
PRESS RTO FIELD DATA SHEETS



EPA Method 2 Field Data Sheet

Drawing of Test Site

Job LP - HAYWARD
Source DROSS RTD OUTLET STACK
Test 1 Run 0 Date 6-7-94
Stack Dimen. 75.5 IN.
Dry Bulb 240 °F Wet bulb 110 °F
Manometer ☒ Reg. ☐ Exp ☐ Elec.
Barometric Pressure 28.73 IN.HG
Static Pressure - 0.30 IN.WC
Operators SB + EJ
Pitot No. 224-8 C. -990



CH₂D IPS

Traverse Point No.	Fraction of Diameter	Distance From Stack Wall (IN.)	Distance From End of Port (IN.)	Velocity	Temp. of Gas (°F)
		Port Length: 6-375 IN.		Time Start:	HRS
A - 1	.026	1.96	8.34		
2	.082	6.19	12.57		
3	.146	11.02	17.74		
4	.226	17.06	23.44		
5	.342	25.82	32.20		
6	.658	49.68	56.05		
7	.774	58.44	64.81		
8	.854	64.48	70.85		
9	.918	69.31	75.68		
10	.974	73.54	79.91		
B - 1					
2					
3					
4					
5					
6					
7					
8					
9					
10					
Temp. Meas. Device & S/N: Digital TC - POT29				Time End:	HRS

R or nothing = reg. manometer; S = expanded; E = electronic

032594-G:STACK\WP\FORMS\5-392.1

INTERPOL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job LP-HAYWARD
Source PROSS RTD OUTLET STACK
Method 001 Filter holder: N/A
Sample Train Leak Check:

Date 6-7-94 Test 1 Run 1
No. of traverse points 20
Filter type: N/A

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
Post test: 0.005 cfm at 17 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

N/A

Recovery solvent(s)

☐ acetone
☒ other(s) MELLS

No. of probe wash bottles:

Sample recovered by:

1
SB + EJ

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2	<u>484</u>	<u>479</u>	<u>5</u>
Impinger No. 3			
Condenser			
Desiccant	<u>1567</u>	<u>1547</u>	<u>20</u>
Total			<u>25</u>

Integrated Gas Sampling Data:

Bag Pump No. 223
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check: 00
Time start: 1250
Sampling rate: 400

Box No. 26 Bag No. 1
Size: 44 L
cc/min at 15 in. Hg.
(HRS) Time end: 1352 (HRS)
cc/min Operator: SB

S/N of O₂ Analyzer used to monitor train outlet: 11

123093-GASTACK\WP\METHODS\0046RR

INTERPOLL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job LP- HAYWARD Date 6-7-94 Test 1 Run 2
Source PRESS AIR OUTLET STACK No. of traverse points 20
Method 0011 Filter holder: N/A Filter type: N/A
Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
Post test: 0.005 cfm at 14 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

N/A

Recovery solvent(s)

☐ acetone
☒ other(s) MeCL₂

No. of probe wash bottles:

Sample recovered by:

1
SB+ET

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2	<u>510</u>	<u>500</u>	<u>10</u>
Impinger No. 3			
Condenser			
Desiccant	<u>1508</u>	<u>1494</u>	<u>14</u>
Total			<u>24</u>

Integrated Gas Sampling Data:

Bag Pump No. 22B
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check: 00
Time start: 1420
Sampling rate: 400

Box No. 26 Bag No. 2
Size: 44 L
cc/min at 15 in. Hg.
(HRS) Time end: 1522 (HRS)
cc/min Operator: SB

S/N of O₂ Analyzer used to monitor train outlet:

11

123093-GASTACK\WP\METHODS\S-0046RR

CP - MAYWARD

1000	CP - PLAYWRIGHT
1001	PRESS INTO OUTLET STACK
1002	6-7-94 1001 1001 2

Optical Box

$$\frac{11x}{13x + 25}$$

26-111-

Pilot No. 230-8
Bar. Press. 28.2
Velocity No.

0/8

[illegible]

INTERPOLL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job LP - HAYWARD Date 6-7-94 Test 1 Run 3
Source PROFS RTO OUTLET STACK No. of traverse points 20
Method 0011 Filter holder: N/A Filter type: N/A
Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
Post test: 0.00 cfm at 15 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

N/A

Recovery solvent(s)

☐ acetone
☒ other(s) MCCl₄

No. of probe wash bottles:

1

Sample recovered by:

SB-RST

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2	495	478	17
Impinger No. 3			
Condenser			
Desiccant	1536	1519	17
Total			34

Integrated Gas Sampling Data:

Bag Pump No. 223
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check: 00
Time start: 1545
Sampling rate: 400

Box No. 26 Bag No. 3
Size: 44 L
cc/min at 15 in. Hg.
(HRS) Time end: 1646 (HRS)
cc/min Operator: 53

S/N of O₂ Analyzer used to monitor train outlet: 11

123093-GASTACK\WP\METHODS\S-0046RR

INTERPOL LABORATORIES - LA METODO 5 FIELD DATA SHEET

1001 LD- HAYWARD
 1002 ADDRESS RTO OUTLET STAGE
 1003 6-7-54 1001 RUN 3
 Operator 53+KJ
 Meter Box No. 14 MIN 1.85 IN DC
 Generator output. 100%

P101 No. 225-8 Cp -940
 But. Pressure. 22.73 IN HG
 HORIZAL No. 57-7 HORIZAL DIA. 220 IN.

[illegible]

INTERPOL LABORATORIES, INC.
(612) 786-6020
EPA Method 2 Field Data Sheet

Drawing of Test Site

Job LP - HAYWARD

Source PAVSS RTG OUTLET STATIC

Test 2 Run 0 Date 6-8-94

Stack Dimen. 75.5 IN.

Dry Bulb 84.2 °F Wet bulb 109 °F

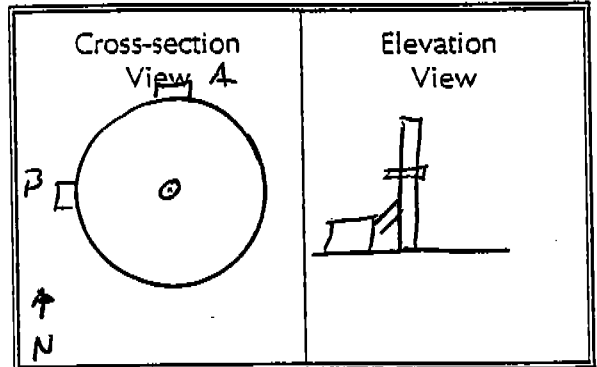
Manometer ☒ Reg. ☐ Exp ☐ Elec.

Barometric Pressure 28.98 IN.HG

Static Pressure - 0.35 IN.WC

Operators SB + RJ

Pitot No. 020-8 C₂ - 840



Traverse Point No.	Fraction of Diameter	Distance From Stack Wall (IN.)	Distance From End of Port (IN.)	Velocity	Temp. of Gas (°F)
		Port Length: 6.375 IN.	Time Start: HRS		
A - 1	.026	1.96	8.34		
2	.082	6.19	12.57		
3	.146	11.02	17.40		
4	.226	17.06	23.44		
5	.342	25.82	32.20		
6	.658	49.68	56.05		
7	.774	58.44	64.81		
8	.854	64.48	70.85		
9	.918	69.31	75.68		
10	.974	73.54	79.91		
B - 1					
2					
3					
4					
5					
6					
7					
8					
9					
10					
Temp. Meas. Device & S/N: DIGITAL TC - PDI 29				Time End: HRS	

R or nothing = reg. manometer; S = expanded; E = electronic

032594-G:STACK\WP\FORMS\S-392.1

INTERPOLL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job LP-HAYWARD Date 6-8-94 Test 2 Run 1
Source PRESS. OUTLET STACK No. of traverse points 20
Method MDI Filter holder: N/A Filter type: N/A
Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
Post test: 0.00 cfm at 7 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

N/A

Recovery solvent(s)

~~Acetone~~ TOLUENE
~~Ether(s)~~ ACETONITRILE

No. of probe wash bottles:

Sample recovered by:

SB + ET

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2	<u>510</u>	<u>494</u>	<u>16</u>
Impinger No. 3			
Condenser			
Desiccant	<u>1544</u>	<u>1534</u>	<u>10</u>
Total			<u>26</u>

Integrated Gas Sampling Data:

Bag Pump No. 223
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check: 00
Time start: 0815
Sampling rate: 400

Box No. 24 Bag No. 1
Size: 44 L
cc/min at 15 in. Hg.
(HRS) Time end: 0916 (HRS)
cc/min Operator: 53

S/N of O₂ Analyzer used to monitor train outlet:

11

116 LP-FLAVNARD

LP- HAYWARD
PRESS RTO OUTLET STACK
6-8-97 1001 @ NON

1. **James M. Smith**
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 76. **James M. Smith**
 77. **James M. Smith**
 78. **James M. Smith**
 79. **James M. Smith**
 80. **James M. Smith**
 81. **James M. Smith**
 82. **James M. Smith**
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 92. **James M. Smith**
 93. **James M. Smith**
 94. **James M. Smith**
 95. **James M. Smith**
 96. **James M. Smith**
 97. **James M. Smith**
 98. **James M. Smith**
 99. **James M. Smith**
 100. **James M. Smith**

513-6J
14 1111 1
1.006

20-11-3

Pitot No.	220-8
Bar. Pres.	28.9
Worley No.	67-4

068

[illegible]

INTERPOLL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job LP - HAYWARD Date 6-8-94 Test 2 Run 2
Source PROSS RD OUTLET STACK No. of traverse points 20
Method MDF Filter holder: N/A Filter type: N/A
Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
Post test: 0.00 cfm at 7 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

Recovery solvent(s)

N/A

~~X~~ acetone ACETONITRILE
~~X~~ other(s) TOLUENE

No. of probe wash bottles:

Sample recovered by:

SB

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2	<u>527</u>	<u>510</u>	<u>17</u>
Impinger No. 3			
Condenser			
Desiccant	<u>1520</u>	<u>1510</u>	<u>10</u>
Total			<u>27</u>

Integrated Gas Sampling Data:

Bag Pump No. 223
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check: 00
Time start: 0945
Sampling rate: 400

Box No. 24 Bag No. 2
Size: 44 L
cc/min at 15 in. Hg.
(HRS) Time end: 1046 (HRS)
cc/min Operator: SB

S/N of O₂ Analyzer used to monitor train outlet: 11

123093-G:\STACK\WP\METHODS\S-0046RR

INTERPOLL LABDRATORIES EPA METHOD 5 FIELD DATA SHEET

106 LP - FORWARD

100	LP - HAYWARD
100	PROS. RTO 2707 5746
100	5-8-94 1001 2 NOV 2

1970

SP + EJ
79

425-11116

P

$\frac{1.75}{1.8}$
 $\frac{1.75}{1.8}$
 $\frac{1.75}{1.8}$

10 417 100
Cp 444 3

0211
07.8

[illegible]

INTERPOLL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job LP - HAYWARD Date 6-8-94 Test 2 Run 3
Source PRV. PTO OUTLET STAIR No. of traverse points 20
Method N/A Filter holder: N/A Filter type: N/A
Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
Post test: 0.00 cfm at 8 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

N/A

Recovery solvent(s)

~~Solvent~~ ACETONE
Other(s) TOLUENE

No. of probe wash bottles:

Sample recovered by:

SP + ES

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2	503	490	13
Impinger No. 3			
Condenser			
Desiccant	1520	1510	10
Total			23

Integrated Gas Sampling Data:

Bag Pump No. 223
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check: 00
Time start: 1115
Sampling rate: 400

Box No. 24 Bag No. 3
Size: 44 L
cc/min at 15 in. Hg.
(HRS) Time end: 1216 (HRS)
cc/min Operator: SB

S/N of O₂ Analyzer used to monitor train outlet:

11

123093-G:STACK\WPMETHODS\5-0046RR

INTERPOL LABORATORIES EPA METHOD 5 FIELD DATA SHEET

Source: PROS, PRO 0
6-8-84
LP - HAYWARD

106
500
1000
1000
7

LP - MAYNARD
PROSS PRO OFFICE STAGE

1000 2 1981 6-8-81

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 ১৯৩৬ ১৯৩৭ ১৯৩৮ ১৯৩৯ ১৯৪০
 ১৯৪১ ১৯৪২ ১৯৪৩ ১৯৪৪ ১৯৪৫

1006
1111
SB + EI

2011-987

P. 1. H.
B. 1. J.
H. 1. J.

8-22

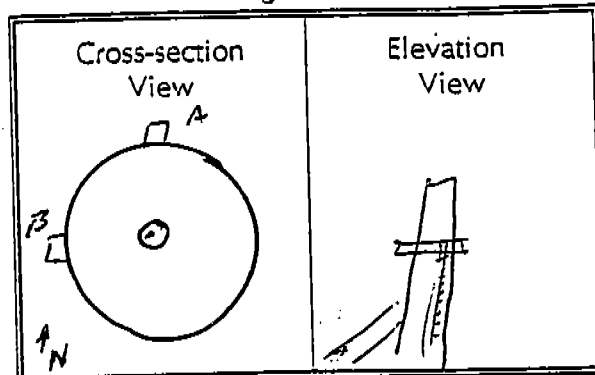
0211 5111 43
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INTERPOLL LABORATORIES, INC.
(612) 786-6020
EPA Method 2 Field Data Sheet

Drawing of Test Site

Job LP - HAYWARD
Source #1 PROCESS RTO OUTLET
Test 3 Run 0 Date 6-10-94
Stack Dimen. 25.5 IN.
Dry Bulb 241 °F Wet bulb 110 °F
Manometer ☒ Reg. ☐ Exp ☐ Elec.
Barometric Pressure 28.93 IN.HG
Static Pressure - .43 IN.WC
Operators SB + ES
Pitot No. 220-8 C_p .840



Traverse Point No.	Fraction of Diameter	Distance From Stack Wall (IN.)	Distance From End of Port (IN.)	Velocity	Temp. of Gas (°F)
		Port Length: <u>6.375</u> IN.		Time Start: <u>0837</u> HRS	
A - 1	.026	1.90	8.34	.40	250
2	.082	6.19	12.57	.48	251
3	.146	11.02	17.40	.38	251
4	.226	17.06	23.44	.60	251
5	.342	25.82	32.20	.63	251
6	.658	49.68	56.05	.65	254
7	.771	59.40	64.91	.60	253
8	.854	64.48	70.85	.65	252
9	.918	69.31	75.68	.66	251
10	.974	73.57	79.91	.63	254
B - 1				.42	252
2				.54	252
3				.63	252
4				.61	252
5				.63	251
6				.68	251
7				.66	251
8				.69	251
9				.69	251
10				.69	251
		ACFM =	97,064		
		ASCFM =	67,437		
		FT/sec =	52.03		
		SCFM =	60,000	69,164	
Temp. Meas. Device & S/N: <u>Digital TC-PDT 29</u>				Time End:	HRS

R or nothing = reg. manometer; S = expanded; E = electronic

032594-G:\STACK\WP\FORMS\S-392.1

INTERPOLL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job LP-HAYWARD Date 6-10-84 Test 3 Run 1
Source #1 PROCESS RO OUTLET No. of traverse points 20
Method 1.5 Filter holder: GLASS Filter type: 4" G.F.
Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
Post test: 0.00 cfm at 10 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

4041

Recovery solvent(s)

☒ acetone _____
☐ other(s) _____

No. of probe wash bottles:

Sample recovered by:

1
SB

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2	<u>507</u>	<u>498</u>	<u>9</u>
Impinger No. 3			
Condenser			
Desiccant	<u>1455</u>	<u>1440</u>	<u>15</u>
Total			<u>24</u>

Integrated Gas Sampling Data:

Bag Pump No. 22B
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check: 00
Time start: 0935
Sampling rate: 400

Box No. 19 Bag No. 1
Size: 44 L
cc/min at 15 in. Hg.
(HRS) Time end: 1036 (HRS)
cc/min Operator: SB

S/N of O₂ Analyzer used to monitor train outlet: 11

123093-GASTACKIWP\METHODS\IS-0046RR

[illegible]

C-17

INTERPOLL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job LP-HOYWARD Date 6-10-84 Test 3 Run 2
Source #1 PROCESS AIR OUTLET No. of traverse points 20
Method 1-5 Filter holder: 4" GLASS Filter type: 4" GLASS FIBER
Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
Post test: 0.00 cfm at 15 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

4044

Recovery solvent(s)

☒ acetone
☐ other(s)

No. of probe wash bottles:

1
SB+EJ

Sample recovered by:

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2	<u>526</u>	<u>513</u>	<u>13</u>
Impinger No. 3			
Condenser			
Desiccant	<u>1535</u>	<u>1519</u>	<u>16</u>
Total			<u>29</u>

Integrated Gas Sampling Data:

Bag Pump No. 223
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check: 00
Time start: 1100
Sampling rate: 400

Box No. 19 Bag No. 2
Size: 44 L
cc/min at 15 in. Hg.
(HRS) Time end: 1201 (HRS)
cc/min Operator: SB

S/N of O₂ Analyzer used to monitor train outlet:

11

123093-GASTACK\WPMETHODS\0046RR

INTERPOL LABORATORIES A METHOD 5 FIELD DATA SHEET

[illegible][illegible]

INTERPOL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job LP-HAYWARD Date 6-10-74 Test 3 Run 3
Source #1 PRESS INTO OUTLET No. of traverse points 20
Method 1-5 Filter holder: 4" glass Filter type: 4" glass fiber
Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
Post test: 0.22 cfm at 12 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

4043

Recovery solvent(s)

☒ acetone _____
☐ other(s) _____

No. of probe wash bottles:

Sample recovered by:

1
SB + 18J

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2	514	500	14
Impinger No. 3			
Condenser			
Desiccant	1534	1520	14
Total			28

Integrated Gas Sampling Data:

Bag Pump No. 22B
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check: 00
Time start: 1220
Sampling rate: 400

Box No. 19 Bag No. 3
Size: 44 L
cc/min at 15 in. Hg.
(HRS) Time end: 1721 (HRS)
cc/min Operator: SB

S/N of O₂ Analyzer used to monitor train outlet:

11

123093-GASTACKWPMETHODSIS-0046RR

INTERPOL LABORATORIES A METHOD 5 FIELD DATA SHEET

LP- HAYWARD

60100	41	DRON	ATO	OUTER	3	400	3
60100	6	63-74	1061	3	400	3	3

Dd Jj Bb
 Hh Tt Xx

SB + EJ
14 MIN 2.85 IN DE
1.0059

11 12 13 14 15 16 17 18 19 20 21 22 23 24 25 26 27 28 29 30 31 32 33 34 35 36 37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57 58 59 60 61 62 63 64 65 66 67 68 69 70 71 72 73 74 75 76 77 78 79 80 81 82 83 84 85 86 87 88 89 90 91 92 93 94 95 96 97 98 99 100 101 102 103 104 105 106 107 108 109 110 111 112 113 114 115 116 117 118 119 120 121 122 123 124 125 126 127 128 129 130 131 132 133 134 135 136 137 138 139 140 141 142 143 144 145 146 147 148 149 150 151 152 153 154 155 156 157 158 159 160 161 162 163 164 165 166 167 168 169 170 171 172 173 174 175 176 177 178 179 180 181 182 183 184 185 186 187 188 189 190 191 192 193 194 195 196 197 198 199 200 201 202 203 204 205 206 207 208 209 210 211 212 213 214 215 216 217 218 219 220 221 222 223 224 225 226 227 228 229 230 231 232 233 234 235 236 237 238 239 240 241 242 243 244 245 246 247 248 249 250 251 252 253 254 255 256 257 258 259 260 261 262 263 264 265 266 267 268 269 270 271 272 273 274 275 276 277 278 279 280 281 282 283 284 285 286 287 288 289 290 291 292 293 294 295 296 297 298 299 300 301 302 303 304 305 306 307 308 309 310 311 312 313 314 315 316 317 318 319 320 321 322 323 324 325 326 327 328 329 330 331 332 333 334 335 336 337 338 339 340 341 342 343 344 345 346 347 348 349 350 351 352 353 354 355 356 357 358 359 360 361 362 363 364 365 366 367 368 369 370 371 372 373 374 375 376 377 378 379 380 381 382 383 384 385 386 387 388 389 390 391 392 393 394 395 396 397 398 399 400 401 402 403 404 405 406 407 408 409 410 411 412 413 414 415 416 417 418 419 420 421 422 423 424 425 426 427 428 429 430 431 432 433 434 435 436 437 438 439 440 441 442 443 444 445 446 447 448 449 450 451 452 453 454 455 456 457 458 459 460 461 462 463 464 465 466 467 468 469 470 471 472 473 474 475 476 477 478 479 480 481 482 483 484 485 486 487 488 489 490 491 492 493 494 495 496 497 498 499 500 501 502 503 504 505 506 507 508 509 510 511 512 513 514 515 516 517 518 519 520 521 522 523 524 525 526 527 528 529 530 531 532 533 534 535 536 537 538 539 540 541 542 543 544 545 546 547 548 549 550 551 552 553 554 555 556 557 558 559 560 561 562 563 564 565 566 567 568 569 570 571 572 573 574 575 576 577 578 579 580 581 582 583 584 585 586 587 588 589 590 591 592 593 594 595 596 597 598 599 600 601 602 603 604 605 606 607 608 609 610 611 612 613 614 615 616 617 618 619 620 621 622 623 624 625 626 627 628 629 630 631 632 633 634 635 636 637 638 639 640 641 642 643 644 645 646 647 648 649 650 651 652 653 654 655 656 657 658 659 660 661 662 663 664 665 666 667 668 669 670 671 672 673 674 675 676 677 678 679 680 681 682 683 684 685 686 687 688 689 690 691 692 693 694 695 696 697 698 699 700 701 702 703 704 705 706 707 708 709 710 711 712 713 714 715 716 717 718 719 720 721 722 723 724 725 726 727 728 729 730 731 732 733 734 735 736 737 738 739 740 741 742 743 744 745 746 747 748 749 750 751 752 753 754 755 756 757 758 759 760 761 762 763 764 765 766 767 768 769 770 771 772 773 774 775 776 777 778 779 780 781 782 783 784 785 786 787 788 789 790 791 792 793 794 795 796 797 798 799 800 801 802 803 804 805 806 807 808 809 810 811 812 813 814 815 816 817 818 819 820 821 822 823 824 825 826 827 828 829 830 831 832 833 834 835 836 837 838 839 840 841 842 843 844 845 846 847 848 849 850 851 852 853 854 855 856 857 858 859 860 861 862 863 864 865 866 867 868 869 870 871 872 873 874 875 876 877 878 879 880 881 882 883 884 885 886 887 888 889 890 891 892 893 894 895 896 897 898 899 900 901 902 903 904 905 906 907 908 909 910 911 912 913 914 915 916 917 918 919 920 921 922 923 924 925 926 927 928 929 930 931 932 933 934 935 936 937 938 939 940 941 942 943 944 945 946 947 948 949 950 951 952 953 954 955 956 957 958 959 960 961 962 963 964 965 966 967 968 969 970 971 972 973 974 975 976 977 978 979 980 981 982 983 984 985 986 987 988 989 990 991 992 993 994 995 996 997 998 999 1000 1001 1002 1003 1004 1005 1006 1007 1008 1009 1010 1011 1012 1013 1014 1015 1016 1017 1018 1019 1020 1021 1022 1023 1024 1025 1026 1027 1028 1029 1030 1031 1032 1033 1034 1035 1036 1037 1038 1039 1040 1041 1042 1043 1044 10

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7.5

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12
13

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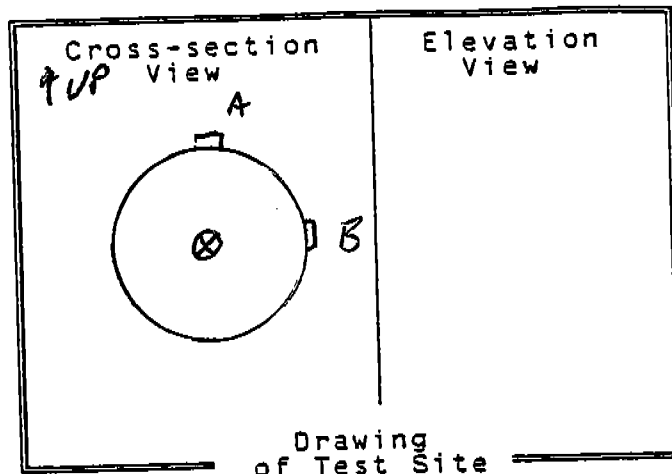
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Visible Emissions Form

13

SOURCE NAME <u>L. D. Hayward</u>			OBSERVATION DATE <u>6-10-94</u>			START TIME <u>11:00</u>			STOP TIME <u>12:00</u>			
ADDRESS <u>Line 1 Press RTO STACK OUTLET</u>			SEC MIN	0	15	30	45	SEC MIN	0	15	30	45
<u>May 63</u>			1	0	0	0	0	31	0	0	0	0
CITY <u>Hayward</u>	STATE <u>CA</u>	ZIP	2	0	0	0	0	32	0	0	0	0
PHONE <u>1</u>	SOURCE ID NUMBER		3	0	0	0	0	33	0	0	0	0
PROCESS EQUIPMENT <u>Line 1 Press</u>		OPERATING MODE <u>100%</u>	4	0	0	0	0	34	0	0	0	0
CONTROL EQUIPMENT <u>RTO</u>		OPERATING MODE <u>100%</u>	5	0	0	0	0	35	0	0	0	0
DESCRIBE EMISSION POINT <u>Return Smoke Stack</u>			6	0	0	0	0	36	0	0	0	0
START <u>Same</u> STOP <u>Same</u>			7	0	0	0	0	37	0	0	0	0
HEIGHT ABOVE GROUND LEVEL START <u>100'</u> STOP <u>Same</u>			8	0	0	0	0	38	0	0	0	0
HEIGHT RELATIVE TO OBSERVER START <u>100'</u> STOP <u>Same</u>			9	0	0	0	0	39	0	0	0	0
DISTANCE FROM OBSERVER START <u>400'</u> STOP <u>Same</u>			10	0	0	0	0	40	0	0	0	0
DIRECTION FROM OBSERVER START <u>NNW</u> STOP <u>Same</u>			11	0	0	0	0	41	0	0	0	0
DESCRIBE EMISSIONS START <u>N/A</u> STOP <u>N/A</u>			12	0	0	0	0	42	0	0	0	0
EMISSION COLOR START <u>N/A</u> STOP <u>N/A</u>			13	0	0	0	0	43	0	0	0	0
PLUME TYPE: CONTINUOUS ☐ FUGITIVE ☐ INTERMITTENT ☐			14	0	0	0	0	44	0	0	0	0
WATER DROPLETS PRESENT: NO ☒ YES ☐			15	0	0	0	0	45	0	0	0	0
IF WATER DROPLET PLUME: ATTACHED ☐ DETACHED ☐			16	0	0	0	0	46	0	0	0	0
POINT IN THE PLUME AT WHICH OPACITY WAS DETERMINED START <u>1' above stack</u> STOP <u>Same</u>			17	0	0	0	0	47	0	0	0	0
DESCRIBE BACKGROUND START <u>SKY</u> STOP <u>Same</u>			18	0	0	0	0	48	0	0	0	0
BACKGROUND COLOR START <u>BLUE</u> STOP <u>BLUE</u>			19	0	0	0	0	49	0	0	0	0
SKY CONDITIONS START <u>Clear</u> STOP <u>Same</u>			20	0	0	0	0	50	0	0	0	0
WIND SPEED START <u>0-5</u> STOP <u>Same</u>			21	0	0	0	0	51	0	0	0	0
WIND DIRECTION START <u>SW</u> STOP <u>Same</u>			22	0	0	0	0	52	0	0	0	0
AMBIENT TEMP. START <u>72</u> STOP <u>Same</u>			23	0	0	0	0	53	0	0	0	0
WET BULB TEMP. <u>52</u>			24	0	0	0	0	54	0	0	0	0
RH, percent <u>59%</u>			25	0	0	0	0	55	0	0	0	0
			26	0	0	0	0	56	0	0	0	0
			27	0	0	0	0	57	0	0	0	0
			28	0	0	0	0	58	0	0	0	0
			29	0	0	0	0	59	0	0	0	0
			30	0	0	0	0	60	0	0	0	0
			AVERAGE OPACITY FOR HIGHEST PERIOD			NUMBER OF READINGS ABOVE % WERE						
RANGE OF OPACITY READINGS MINIMUM			MAXIMUM									
OBSERVER'S NAME (PRINT) <u>DAVID VANDER</u>												
OBSERVER'S SIGNATURE <u>David Vander</u>			DATE <u>6-10-94</u>									
ORGANIZATION <u>INTERPOLL LABORATORIES</u>												
I HAVE RECEIVED A COPY OF THESE OPACITY OBSERVATIONS SIGNATURE			DATE <u>4-6-94</u>									
TITLE			DATE									
DATE			VERIFIED BY									
			DATE									

Job L.P. / Hayward, WI
 Source Line 1 Press PTO / Inlet
 Test 5 Run 0 Date 6-10-94
 Stack dimen. 53.125 IN.
 Dry bulb 120 °F Wet bulb 75 °F
 Manometer: ☒ Reg. ☐ Exp. ☐ Elec.
 Barometric pressure 28.93 in Hg
 Static pressure -2.95 in WC
 Operators M. Kachler + D. Vacker + K.N.
 Pitot No. 246-B C, 04



Traverse Point No.	Fraction of Diameter	Distance from Stack Wall (in)	Distance from End of Port (in)	Velocity Pressure (in WC)	Temperature of gas (°F)
Port length: <u>6.375</u> in.				Time start: <u>0941</u> hrs	
A-1				<u>1.58</u>	
2				<u>1.75</u>	
3				<u>1.50</u>	
4				<u>1.48</u>	
5				<u>1.32</u>	
6				<u>1.44</u>	
7				<u>1.58</u>	
8				<u>1.60</u>	
9				<u>1.70</u>	
10				<u>1.77</u>	
11				<u>1.72</u>	
12				<u>1.75</u>	<u>116</u>
B-1				<u>1.37</u>	
2				<u>1.40</u>	
3				<u>1.48</u>	
4	<u>B = 13" 22"</u>			<u>1.37</u>	
5	<u>A = 257"</u>			<u>1.40</u>	
6				<u>1.32</u>	
7				<u>1.36</u>	
8	<u>ACFM</u>	<u>67,252</u>		<u>1.33</u>	
9	<u>DS CFM</u>	<u>57,386</u>		<u>1.24</u>	
10	<u>FT/SEC</u>	<u>72.14</u>		<u>1.05</u>	
11	<u>SCFM</u>	<u>59,078</u>	<u>58,775</u>	<u>1.18</u>	
12				<u>1.10</u>	
Temp. meas. device & S/N: <u>PDT-31 / TC</u>				Time end: <u>0947</u> hrs	

INTERPOLL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job L.P. / Hayward, CA Date 6-10-94 Test 5 Run 1
Source Line / Press 120 / Inlet No. of traverse points 24
Method 5 Filter holder: Reflex Filter type: 3.52" pull flex
Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
Post test: 0.02 cfm at 10 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

1318

Recovery solvent(s)

☒ Acetone

☐ other(s)

No. of probe wash bottles:

1

Sample recovered by:

M. Kasper + K. Nuerstner

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2	<u>498</u>	<u>498</u>	<u>-</u>
Impinger No. 3			
Condenser			
Desiccant	<u>1509</u>	<u>1490</u>	<u>19</u>
Total			<u>19</u>

Integrated Gas Sampling Data: NA / Ambient

Bag Pump No. _____
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check: _____
Time start: _____
Sampling rate: _____

Box No. _____ Bag No. _____
Size: 44 L
cc/min at _____ in. Hg.
(HRS) Time end: _____ (HRS)
cc/min Operator: _____

S/N of O₂ Analyzer used to monitor train outlet: _____

123093-GASTACKWP\METHODS\IS-0046RR

[illegible][illegible]

INTERPOLL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job L.P. / Hayward, CA Date 6/10/94 Test 5 Run 2
Source Line 1 Press RTD / Inlet No. of traverse points 24
Method 5 Filter holder: Teflon Filter type: 3.52" Pallflex
Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
Post test: 0.00 cfm at 10 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

1319

Recovery solvent(s)

☒ Acetone
☐ Other(s)

No. of probe wash bottles:

Sample recovered by:

1
M. Kachler + R. Bressmerer

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2	407	400	7
Impinger No. 3			
Condenser			
Desiccant	1435	1417	18
Total			25

Integrated Gas Sampling Data: NA / Ambient

Bag Pump No. _____
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check: _____
Time start: _____
Sampling rate: _____

Box No. _____ Bag No. _____
Size: 44 L
cc/min at _____ in. Hg.
(HRS) Time end: _____ (HRS)
cc/min Operator: _____

S/N of O₂ Analyzer used to monitor train outlet: _____

123093-GASTACK\WPMETHODS\0046RR

Operator Mr. Kachulak Pilot No. 24V-8 Ep 04
 Motor Box No. 9 1.78 IN DE Bar. Press. 28.93 IN HG 120 2
 Recorder count. 996 Horiz. No. 24V-3 Horiz. No. 016 08 11

Operator Mr. Kachulak Pilot No. 24V-8 Ep 04
 Motor Box No. 9 1.78 IN DE Bar. Press. 28.93 IN HG 120 2
 Recorder count. 996 Horiz. No. 24V-3 Horiz. No. 016 08 11

[illegible]

20.02	2.04
-------	------

$09 = 0$

11-11-11

S-0037R

INTERPOLL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job L.P. / Hayward, WI Date 6-10-94 Test 5 Run 3
Source Line 1 Press RTO / Inlet No. of traverse points 24
Method 5 Filter holder: DeFlon Filter type: 2.52" Pall Fluo
Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
Post test: 0.02 cfm at 15 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

1320

Recovery solvent(s)

☒ Acetone
☐ other(s)

No. of probe wash bottles:

Sample recovered by:

1
M. Koshlora + K. Wossman

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2	399	397	2
Impinger No. 3			
Condenser			
Desiccant	1830	1809	21
Total			23

Integrated Gas Sampling Data: NA / Ambient

Bag Pump No. _____
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check: _____
Time start: _____
Sampling rate: _____

Box No. _____ Bag No. _____
Size: 44 L
cc/min at _____ in. Hg.
(HRS) Time end: _____ (HRS)
cc/min Operator: _____

S/N of O₂ Analyzer used to monitor train outlet: _____

123093-GASTACKIWP/METHODS-0046RR

INTERPOL LABORATORIES EPA METHOD 5 FIELD DATA SHEET

Job h.p. / Hayward, CA
 Source Line / Press 100
 Date 6-10-94
 Operator McKachlagh
 Motor Box No. 128
 Computer Conf. 961
 Pilot No. 240-8
 Bar. Press. 20.93
 Nozzle No. 200-3
 Di. 1/8"
 InHg 20.93
 H₂O 2.15
 In. 1.96

Traverse Point No.	Sampling Time (min)	Sample Volume (cf)	Velocity Head (inH ₂ O)	Drifts Meter (inH ₂ O)	Det. Vol. (cf)	VAC. inHg	Temperature (°F)					Oxygen (xv/v)	
							Stack	Probe	Oven	Ingy.	Gas/In		Gas/Out
A-12	12.0	61.90	1.72	2.04	3.98	8	123	233	247	47	88	86	20.9
11	5	63.95	1.93	2.29	6.18	9	123				90	87	
10	7.5	66.24	1.90	2.26	8.38	9	122	236	250	46	92	87	
9	10	68.42	1.86	2.23	0.56	9	126				93	87	
8	12.5	70.52	1.70	2.03	2.64	8	124	242	253	46	93	88	
7	15	72.58	1.55	1.65	4.63	8	124				93	88	
6	12.5	74.70	1.40	1.67	6.52	7	125	241	255	46	94	88	
5	10	76.64	1.61	1.92	8.54	8	126				95	88	
4	12.5	78.60	1.80	2.14	0.68	8.5	126	238	252	46	95	88	
3	25	80.82	1.68	1.99	1.74	8	129				95	89	
2	27.5	82.90	1.60	1.90	4.76	7.5	127	240	253	47	96	88	
1	30	84.90	1.58	1.88	6.77	7.5	127				95	89	
B-12	31.5	86.80	1.35	1.61	8.63	6.5	127	244	258	47	94	88	
11	35	88.75	1.72	2.04	0.72	8.5	127				96	89	
10	37.5	90.83	1.58	1.88	2.73	8	126	247	255	47	96	90	
9	40	92.88	1.70	2.02	4.81	8.5	128				97	89	
8	42.5	94.91	1.76	2.09	6.93	8.5	128	250	254	49	97	90	
7	45	96.98	1.60	1.90	8.95	8	129				97	89	
6	47.5	98.98	1.73	2.06	1.06	8.5	126	248	251	49	98	90	
5	50	101.10	1.71	2.05	3.16	8.5	125				98	90	
4	52.5	103.26	1.75	2.09	5.28	8.5	127	245	252	50	98	90	
3	55	105.39	1.80	2.14	7.43	8.5	128				98	91	
2	57.5	107.53	1.82	2.18	9.59	9	125	243	249	50	98	91	
1	60	109.65	1.38	1.65	1.48	7	127				98	91	
	132.0	111.64											
		58.74		2.00									
	0 = 60												

CH₂O

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job L.P. Hayward Date 6/10/94 Test 12 Run 1
 Source Line 2 Press Vent Rto Stack No. of traverse points 24
 Method 0011 Filter holder: NA Filter type: NA
 Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
 Post test: 0 cfm at 9 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

Recovery solvent(s)

☐ acetone
☒ other(s) MEL₂ & DF H₂O

No. of probe wash bottles:

Sample recovered by:

1
Dust

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2	214	200	14
Impinger No. 3			
Condenser			
Desiccant	1413	1400	13
Total			27

Integrated Gas Sampling Data:

Bag Pump No. 23B
 Bag Material: 5-layer Aluminized Tedlar
 Pretest leak check: 0
 Time start: 0820
 Sampling rate: 400

Box No. 25 Bag No. 1
 Size: 44 L
 cc/min at 14 in. Hg.
 (HRS) Time end: 8915 (HRS)
 cc/min Operator: Dust

S/N of O₂ Analyzer used to monitor train outlet: 24A

INTERPOL LABORATORIES EPA METHOD 3 FIELD DATA SHEET

Job L.P. Hayward Operator DWH & DM Pitot No. 4M5-8 CP 87
 Source Line 2 Press Vent Rto Stack Meter Box No. 6 1.97 IN UC Bar. Press. 28.93 inHg H2O 25.5 X
 Date 6/10/84 Governor Code 13 Run 1 Nozzle No. 0255 Model No. 240 in.

Traverse Point No.	Sampling Time (min)	Sample Volume (cc)	Velocity Head (inH ₂ O)	Drifts Water (inH ₂ O)	Dep. Vol. (cc)	VAC. inHg	Temperature (°F)				Gas In	Gas Out	Oxygen (xv/v)
							Stack	Probe	Oven	App.			
12	08.5	900.30	.82	2.32	2.38	6	240	250	253	51	67	67	20.7
11	3.5	902.41	.89	2.45	4.51	6	254				74	67	20.7
10	7.5	906.63	.92	2.56	6.70	6	252				76	67	20.6
9	10	908.76	.92	2.56	8.89	7	252	254	256	52	81	68	20.4
8	12.5	911.05	.92	2.59	1.10	7	249				84	69	20.7
7	15	913.16	.97	2.72	3.37	7	252				85	69	20.7
6	17.5	915.67	.86	2.39	5.50	7	260	257	256	51	86	70	20.8
5	20	917.50	.80	2.24	7.57	7	258				89	71	20.7
4	22.5	919.56	.73	2.05	9.54	7	258				89	71	20.8
3	25	921.57	.76	1.98	1.49	7	254	256	257	51	91	72	20.8
2	27.5	923.80	.61	1.74	3.31	6	249				93	73	20.8
1	30	925.14	.60	1.72	5.13	6	247				95	73	20.8
B 12	32.5	927.11	.70	2.01	7.10	7	247	258	256	52	89	74	20.7
11	35	929.07	.78	2.20	9.15	7	256				94	75	20.7
10	37.5	931.26	.81	2.31	1.24	7	251				96	76	20.7
9	40	933.20	.83	2.38	3.20	7	238	256	257	52	96	76	20.7
8	42.5	935.65	.83	2.38	5.56	7	250				96	76	20.7
7	45	937.84	.94	2.71	7.85	7	245				98	77	20.8
6	47.5	940.06	.96	2.74	0.15	7	254	258	256	53	98	78	20.8
5	50	942.13	.96	2.45	2.33	7	256				99	78	20.8
4	52.5	944.44	.90	2.56	4.56	7	259				100	79	20.8
3	55	946.19	.93	2.67	6.83	7	253	257	254	54	100	79	20.8
2	57.5	948.79	.80	2.31	8.95	7	249				101	80	20.8
1	60	950.83	.55	1.59	0.71		249				101	80	20.8
	09.8												
	0 = 60	V = 50.53		ΔH = 2.32							Av. = 82.1		

INTERPOLL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job L.P. Hayward Date 6/10/94 Test 12 Run 2
Source Line 12 Press Vent Rio Stack No. of traverse points 24
Method 0011 Filter holder: NA Filter type: NA
Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
Post test: 0 cfm at 10 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

Recovery solvent(s)

☐ acetone
☒ other(s) MeCL₂ + DI H₂O

No. of probe wash bottles:

Sample recovered by:

1
Butt

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2	<u>214</u>	<u>200</u>	<u>14</u>
Impinger No. 3			
Condenser			
Desiccant	<u>1461</u>	<u>1449</u>	<u>12</u>
Total			<u>26</u>

Integrated Gas Sampling Data:

Bag Pump No. 23B Box No. 15 Bag No. 2
Bag Material: 5-layer Aluminized Tedlar Size: 44 L
Pretest leak check: 0 cc/min at 14 in. Hg.
Time start: 0945 (HRS) Time end: 1043 (HRS)
Sampling rate: 400 cc/min Operator: DAH

S/N of O₂ Analyzer used to monitor train outlet: 24A

123093-GASTACK\WPMETHODSIS-0046RR

INTERPOL LABORATORIES EPA METHOD 5 FIELD DATA SHEET

Job L.P. Hayward
 Source Line 2 Press Vent Kto Stack
 Date 6/10/94 1994 12 Mon 2

Operators Don & DM
 Meter Box No. 6 HP 1.97 IN HC
 Gasometer Coeff. .9947

Pilot No. 4M5-8 Cp .84
 Bar. Press. 28.93 inHg H₂O 2.5 K
 Nozzle No. 6455 Nozzle Dia. 2.40 IN.

Traverse Point No.	Sampling Time (min)	Sample Volume (cf)	Velocity Head (inH ₂ O)	Orifice Meter (inH ₂ O)	Dis. Vol. (cf)	VAC. inHg	Temperature (°F)						Drying (x/v)
							Stack	Probe	Duct	Impg.	Gas In	Gas/Dut	
B 12	0941	957.10	.68	1.95	3.03	6	247	260	254	46	81	80	20.6
11	2.5	953.06	.77	2.16	5.06	6	259				88	80	20.5
10	7.5	955.07	.85	2.41	7.21	7	260				92	81	20.5
9	10	959.50	.87	2.47	9.39	7	257	261	256	47	95	81	20.6
8	12.5	961.64	.84	2.40	1.55	7	255				96	81	20.6
7	15	963.91	.94	2.71	3.84	8	250				99	82	20.6
6	17.5	966.14	.91	2.64	6.11	8	247	260	254	49	101	83	20.6
5	20	968.41	.90	2.61	8.36	8	247				102	83	20.7
4	22.5	970.65	.85	2.47	0.56	8	249				103	84	20.6
3	25	972.80	.81	2.32	2.69	8	261	261	256	50	104	84	20.7
2	27.5	974.66	.71	2.04	4.69	8	259				105	85	20.6
1	30	976.50	.56	1.62	6.47	8	256				105	85	20.6
A 12	32.5	978.70	.81	2.36	8.63	8	249	261	257	51	102	86	20.6
11	35	980.90	.90	2.62	0.89	8	249				105	86	20.6
10	37.5	983.20	.90	2.59	3.14	8	260				106	87	20.6
9	40	985.32	.86	2.48	5.35	8	258	257	256	51	107	87	20.5
8	42.5	987.66	.91	2.67	7.64	8	256				107	87	20.5
7	45	990.01	1.0	2.90	6.03	8	265				108	88	20.5
6	47.5	992.46	1.0	2.93	2.43	8	249	256	256	51	109	88	20.5
5	50	994.60	.84	2.47	4.64	8	248				109	88	20.5
4	52.5	996.97	.87	2.53	6.88	8	257				109	89	20.5
3	55	998.99	.75	2.17	8.95	7	261	258	257	52	109	90	20.5
2	57.5	1000.86	.62	1.80	0.81	7	261				109	90	20.5
1	60	1002.63	.50	1.45	2.53	7	261				109	90	20.4
	(1043)												
	0 = 60	V ₀ = 51.53		ΔH = 2.37							Av _{g.} = 93.8		

INTERPOLL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job L.P. Hayward Date 6/10/94 Test 12 Run 3
Source Line 2 Press Vent RTO Stack No. of traverse points 24
Method 6011 Filter holder: NA Filter type: NA
Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
Post test: 0 cfm at 10 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

Recovery solvent(s)

☐ acetone
☒ other(s) MELLS & DI H₂O

No. of probe wash bottles:

Sample recovered by:

DUH

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2	210	200	10
Impinger No. 3			
Condenser			
Desiccant	1422	1413	9
Total			19

Integrated Gas Sampling Data:

Bag Pump No. 23 B Box No. 15 Bag No. 3
Bag Material: 5-layer Aluminized Tedlar Size: 44 L
Pretest leak check: 0 cc/min at 14 in. Hg.
Time start: _____ (HRS) Time end: _____ (HRS)
Sampling rate: 400 cc/min Operator: DUH

S/N of O₂ Analyzer used to monitor train outlet: 24 A

123093-GASTACK\WPMETHODS\0046RR

INTERPOLL LABORATORIES LPA METHOD 5 FIELD DATA SHEET

Job L.P. Hayward
 Source Line 2 Press Vent KTO Stack
 Date 6/10/94 1st 12 Run 3

Operators DWH & DM
 Meter Box No. 6
 Gas meter coeff. 99.1

28.93 IN HC
99.1

Pilot No. 4415-8 Cp 54
 Bar. Pressure 28.93 IN HG
 Nozzle Dia. 2.5 IN.

Traverse Point No.	Sampling Time (min)	Sample Volume (cf)	Velocity Head (in HC)	Drifts Water (in HC)	Des. Vol. (cf)	VAC. (in HG)	Temperature (°F)				Gas Out	Oxygen (XVS)
							Stack	Probe	Duct	Inpy.	Gas In	
A 12	1121	2.92	.79	2.29	5.03	6.5	251	254	256	50	89	20.6
11	2.5	3.04	.89	2.53	7.25	7	259				104	20.6
10	7.5	9.55	.86	2.50	9.47	7	253				108	20.6
9	10	11.86	.96	2.80	11.82	7	253	256	257	50	109	20.6
8	12.5	14.15	.90	2.63	4.10	7	253				110	20.6
7	15	16.40	.90	2.64	6.38	7	253				112	20.6
6	17.5	18.61	.84	2.47	8.59	7	252	256	257	51	113	20.6
5	20	20.61	.73	2.13	0.65	6	259				113	20.6
4	22.5	22.67	.65	1.90	2.59	6	259				113	20.6
3	25	24.70	.69	2.02	4.60	6	259	256	257	57	113	20.6
2	27.5	26.50	.50	1.47	6.31	5	256				113	20.6
1	30	28.20	.57	1.68	8.14	6	254				114	20.6
B 12	32.5	30.37	.75	2.21	0.24	6	254	254	256	51	110	20.6
11	35	32.45	.77	2.24	2.35	6	260				114	20.6
10	37.5	34.64	.88	2.59	4.62	7	255				114	20.6
9	40	36.80	.80	2.35	6.78	7	257	253	253	53	111	20.6
8	42.5	39.13	.94	2.77	9.13	8	254				115	20.6
7	45	41.36	.85	2.51	1.36	8	254				92	20.6
6	47.5	43.58	.93	2.68	3.65	8	255	254	254	53	95	20.6
5	50	46.03	1.0	2.87	6.02	8	258				98	20.6
4	52.5	48.36	.95	2.74	8.33	8	256				99	20.6
3	55	50.46	.80	2.33	0.47	8	253	256	257	53	103	20.6
2	57.5	52.47	.65	1.91	2.41	8	251				106	20.6
1	60	54.55	.77	2.25	4.53	8	255				107	20.6
	1333											
$\theta = 60$		$V = 51.63$		$\Delta H = 1.69$							Avq. = 99.9	

MDI

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

$Pg = -.98$ Diam = 76.25"

Job A.P. Hayward Date 6/9/94 Test 13 Run 1
Source Line #2 Press RTO Stack No. of traverse points 24
Method 1-2PP Filter holder: NA Filter type: NA
Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
Post test: 0.02 cfm at 10 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

Recovery solvent(s)

☐ acetone
☒ other(s) Acetonitrile + Toluene

No. of probe wash bottles:

Sample recovered by:

1
DVH

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2			
Impinger No. 3			
Condenser			
Desiccant			
Total			29

Integrated Gas Sampling Data: - during same time as TSP

Bag Pump No. 1
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check:
Time start:
Sampling rate:

Box No. Bag No.
Size: 44 L
cc/min at in. Hg.
(HRS) Time end: (HRS)
cc/min Operator:

S/N of O₂ Analyzer used to monitor train outlet:

INTERPOLL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job LP/HAYWARD Date 6-9-94 Test 13 Run 2
Source LIND Z PRESS VENT RTO STAC No. of traverse points 24
Method 1-220 Filter holder: KA Filter type: MA
Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
Post test: 0.0 cfm at 7 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

Recovery solvent(s)

☐ acetone _____
☐ other(s) _____

No. of probe wash bottles:

Sample recovered by:

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2			
Impinger No. 3			
Condenser			
Desiccant			
Total			<u>19</u>

Integrated Gas Sampling Data:

Bag Pump No. _____
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check: _____
Time start: _____
Sampling rate: _____

Box No. _____ Bag No. _____
Size: 44 L
cc/min at _____ in. Hg.
(HRS) Time end: _____ (HRS)
cc/min Operator: _____

S/N of O₂ Analyzer used to monitor train outlet: _____

123093-GASTACK\WPMETHODS\0046RR

INTERPUL LABORATORIES A METHOD 5 FIELD DATA SHEET

Job CPI HAYWARD Operator PULL DM Pilot No. 1045-8 CP
 Source (TAE 2 PRESS CONT RTO STAGE Motor Box No. 3 IN UC 2590 100% H2O
 Date 6-9-94 Recorder 1061 13 RUN 2 Nozzle No. 9983 Nozzle Dia. 1.57 IN.

Injection Point No.	Supplying Plug (in)	Supply Volume (cc)	Velocity Head (in H ₂ O)	Orifice Meter (in H ₂ O)	Obs. Vol. (cc)	VAC. (in Hg)	Temperature (°F)				Gas In	Gas Out	Dry Gas
							Stack	Probe	Dye	Temp.			
C-12	1518	277.75	.63	.63	9.13	3	256	257	255	40	86	86	20.5
11	3	279.90	.74	.74	0.63	4	257				87	87	20.5
10	6	280.71	.86	.86	2.25	5	259				91	87	20.5
9	9	282.38	.80	.79	3.80	5	269	255	259	37	93	88	20.6
8	12	283.81	.73	.73	5.29	5	264				95	89	20.5
7	15	285.34	.81	.81	6.86	5	264				96	89	20.6
6	18	286.94	.79	.79	8.42	5	262	256	258	46	97	90	20.5
5	21	288.54	.87	.88	0.06	5	261				97	90	20.6
4	24	290.06	.84	.84	1.67	5	262				97	90	20.6
3	27	291.68	.84	.85	3.28	5	261	257	256	47	99	91	20.6
2	30	293.30	.80	.81	4.86	5	261				99	91	20.6
1	33	294.93	.81	.82	6.44	5	260				99	91	20.6
B-12	36	296.51	.77	.78	7.99	5	261	257	254	48	99	91	20.6
11	39	297.15	.89	.91	9.66	5	252				99	91	20.6
10	42	299.68	.88	.90	1.32	5	252				100	92	20.6
9	45	301.36	.97	.99	3.07	5	252	257	256	49	100	92	20.6
8	48	303.15	.96	.98	4.81	5	253				95	91	20.6
7	51	304.80	.88	.89	6.47	5	253				96	91	20.7
6	54	306.41	.80	.80	8.04	4	263	255	259	48	99	92	20.7
5	57	308.00	.81	.82	9.63	4	260				99	93	20.7
4	60	309.65	.68	.69	1.08	4	261				100	93	20.7
3	63	311.10	.60	.61	2.45	4	261	256	260	49	100	93	20.7
2	66	312.54	.55	.56	3.76	4	258				100	93	20.7
1	69	313.90	.52	.53	5.04		260				100	93	20.7
	72	315.04											
(1641)													
Σ = 72													
V _g = 36.29													
Avg. = 93.7													

INTERPOLL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job LP/HAYWARD Date 6-27-74 Test 13 Run 3
Source LIND Z PRESS VENT RTO STACK No. of traverse points 24
Method 1-2PP Filter holder: NA Filter type: DA
Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
Post test: 0 cfm at 10 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

Recovery solvent(s)

☐ acetone _____
☐ other(s) _____

No. of probe wash bottles:

Sample recovered by:

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2			
Impinger No. 3			
Condenser			
Desiccant			
Total			16

Integrated Gas Sampling Data:

Bag Pump No. _____
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check: _____
Time start: _____
Sampling rate: _____

Box No. _____ Bag No. _____
Size: 44 L
cc/min at _____ in. Hg.
(HRS) Time end: _____ (HRS)
cc/min Operator: _____

S/N of O₂ Analyzer used to monitor train outlet: _____

125093-GASTACK\WP\METHODS\5-0046RR

INTERPOL LABORATORIES "A" METHOD 5 FIELD DATA SHEET

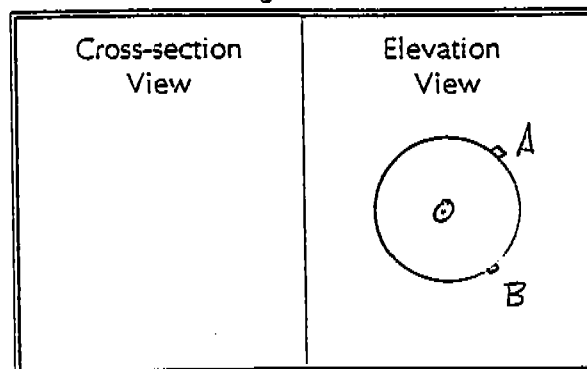
Job L.P. Hayward Operator DW 4ms-8 Ep 87
 Source Line 2 Press Vent 270 Stack Meter Box No. 3 SNP 1.70 IN NC Bar. Pres. 28.90 1019 H2O 25.8
 Date 6/9/74 1051 13 RUN 3 9983 Horiz. No. 685 MDI 10.4 189 11.

Transfer Point No.	Supplying Pipe (in)	Supply Volume (cfs)	Velocity Head (in H ₂ O)	Orifice Meter (in H ₂ O)	Dis. Vol. (cfs)	VAC. (in Hg)	Temperature (°F)					Dryden (xv/v)	
							Stack	Probe	Down	Imp.	Gas In		Gas Out
C-12	17 1/2	315.35	.71	.72	6.83	4	256	237	251	49	89	88	20.4
	3	316.91	.70	.70	8.30	4	255				91	89	20.5
	6	318.50	.89	.90	9.95	4	255				92	89	20.5
	9	319.56	.81	.82	1.53	4	256	253	253	51	93	90	20.5
	15	323.35	.89	.89	3.18	4	263				95	90	20.5
7	18	324.94	.72	.92	4.86	4	263				95	90	20.5
4	21	326.65	.90	.91	6.53	4	257	260	257	51	96	90	20.5
5	24	328.37	.91	.92	8.20	4	260				96	90	20.5
4	27	329.95	.88	.89	9.85	4	258				97	90	20.5
3	30	331.74	.85	.85	1.47	4	262	261	256	52	97	90	20.5
2	33	333.10	.84	.85	3.08	4	261				98	91	20.5
1	36	334.76	.78	.78	4.63	4	262				98	91	20.5
B-12	39	336.26	.76	.76	6.17	4	263	264	257	53	98	91	20.5
	42	337.76	.76	.77	7.70	4	260				98	91	20.5
	45	339.36	.81	.82	9.29	4	260				100	93	20.5
	48	340.99	.86	.87	0.93	4	257	264	257	54	100	93	20.5
	51	342.60	.86	.88	2.58	4	256				101	93	20.5
7	54	344.36	1.0	1.02	4.35	4	255				101	93	20.5
6	57	346.07	1.05	1.07	6.17	4	254	265	260	54	104	95	20.5
5	60	347.91	1.0	1.03	7.95	4	254				104	95	20.5
4	63	349.70	1.0	1.03	9.74	4	251				106	97	20.5
3	66	351.47	.90	.93	1.44	4	254	261	261	54	106	97	20.5
2	69	353.21	.87	.90	3.11	4	253				106	97	20.5
1	72	354.67	.71	.73	4.62		252				106	97	20.5
Σ = 1828							Avg. = 95.3						

INTERPOLL LABORATORIES, INC.
(612) 786-6020
EPA Method 2 Field Data Sheet

Drawing of Test Site

Job L.P. Hayward
Source Line 2 Press Vent Rto Stack
Test 14 Run 6/9/84 Date 6/9/84
Stack Dimen. 76.25 IN.
Dry Bulb °F Wet bulb °F
Manometer ☐ Reg. ☐ Exp ☐ Elec.
Barometric Pressure 28.98 IN.HG
Static Pressure -.98 IN.WC
Operators D. VanHoever & D. Marso
Pitot No. 4M5 C_p .84



Traverse Point No.	Fraction of Diameter	Distance From Stack Wall (IN.)	Distance From End of Port (IN.)	Velocity	Temp. of Gas (°F)
		Port Length: <u>6 1/4</u> IN.	Time Start: <u> </u> HRS		
A 1	.021	1.6	7.85		
2	.067	5.11	11.35		
3	.118	9.0	15.25		
4	.177	13.5	19.75		
5	.250	19.06	25.31		
6	.356	27.14	33.4		
7	.644	49.10	55.36		
8	.750	57.19	63.44		
9	.823	62.75	69		
10	.882	67.25	73.5		
11	.933	71.14	77.39		
12	.979	74.65	80.90		
B 1					
2					
3					
4					
5					
6					
7					
8					
9					
10					
11					
12					
Temp. Meas. Device & S/N:				Time End: <u> </u> HRS	

R or nothing = reg. manometer; S = expanded; E = electronic

032594-G:STACK/WP/FORMS/392.1

INTERPOLL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job L.P. Hayward Date 6/9/94 Test 14 Run 1
Source Line 2 Press Vent RTO Stack No. of traverse points 24
Method 5 Filter holder: glass Filter type: particulate
Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
Post test: 0.00 cfm at 12 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

Recovery solvent(s)

☒ acetone
☐ other(s)

No. of probe wash bottles:

Sample recovered by:

1
DWH

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2	210	200	10
Impinger No. 3			
Condenser			
Desiccant	1435	1419	16
Total			26

Integrated Gas Sampling Data:

Bag Pump No. 2313
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check: 0
Time start: 1246
Sampling rate: 400

Box No. 22 Bag No. 2
Size: 44 L
cc/min at 14 in. Hg.
(HRS) Time end: 1312 (HRS)
cc/min Operator: DWH

S/N of O₂ Analyzer used to monitor train outlet:

24 A

123093-GASTACK\WP\METHODS\5-0046RR

INTERPOL LABORATORIES EPA METHOD 5 FIELD DATA SHEET

Barium Chloride
0.550g

Job L.P. Hayward
Source Black 2 Press Vent Pto Stack
Date 6/9/94 1994 74 Run

Operator Don E. M.
Water Box No. 6
Computer Port 1

Stack 1-77 IN HC
9447

Pilot No. 23-8 Cp 840
Bar. Press. 28.78 inHg H₂O
Nozzle No. glass Nozzle Dia. 2.76 in.

Traverse Point No.	Sampling Time (min)	Sample Volume (cc)	Velocity Head (inH ₂ O)	Drifted Meter (inH ₂ O)	Des. Vol. (cc)	VAD. inHg	Temperature (°F)					Oxygen (X ₂ /V)	
							Stack	Probe	Oven	Inph.	Gas In		Gas Out
A 12	(12:40)	726.40	.77	2.37	8.50	6	250	252	253	48	76	74	20.2
11	5	728.50	.68	2.11	0.49	6	249				77	74	20.1
10	7.5	730.49	.86	2.64	2.72	6	258				80	74	20.1
9	10	732.67	.94	2.90	5.06	8	255	255	248	49	83	75	20.1
8	12.5	735.09	.83	2.57	7.27	7	254				85	75	20.1
7	15	737.20	.93	2.89	9.61	8	254				87	76	20.1
6	17.5	739.58	.95	2.96	1.98	8	254	250	252	47	90	77	20.1
5	20	741.79	.99	3.10	4.41	9	253				91	77	20.1
4	22.5	744.21	.96	3.04	6.82	9	246				92	78	20.0
3	25	746.68	.84	2.66	9.08	8	248	255	260	49	93	78	20.0
2	27.5	749.06	.93	2.94	1.45	8	250				94	79	20.0
1	30	751.36	.98	3.10	3.89	8	249				96	79	20.7
B 12	32.5	753.75	.72	2.29	5.99	7	248	258	261	50	93	80	20.6
11	35	755.91	.73	2.31	8.10	7	251				96	81	20.6
10	37.5	758.02	.83	2.59	0.34	7	262				98	81	20.6
9	40	760.28	.87	2.75	2.64	8	255	257	260	47	99	82	20.6
8	42.5	762.59	.94	2.99	5.04	8	251				100	82	20.6
7	45	764.97	.92	2.89	7.41	8	262				101	83	20.7
6	47.5	767.34	.83	2.67	9.68	8	247	260	258	50	102	83	20.7
5	50	769.67	.87	2.74	1.99	8	262				103	84	20.6
4	52.5	771.95	.75	2.39	4.14	7	255				102	85	20.6
3	55	774.19	.87	2.78	6.47	7	253	261	255	48	103	85	20.6
2	57.5	776.37	.82	2.61	8.72	7	257				104	85	20.6
1	60	778.66	.73	2.36	0.86	6	247				104	86	20.5
	(13:42)	780.83											
	Q = 60	V = 54.43		ΔH = 2.69							avg. = 86.7		

INTERPOLL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job LIP. HAYWARD Date 6/8/94 Test 14 Run 2
Source Line 2 Press Vent Rto Stack No. of traverse points 24
Method 5 Filter holder: glass Filter type: pull/flow
Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
Post test: 402 cfm at 10 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

Recovery solvent(s)

☒ Acetone
☐ other(s)

No. of probe wash bottles:

1
DWH

Sample recovered by:

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1		200	
Impinger No. 2	210		10
Impinger No. 3			
Condenser			
Desiccant	1428	1410	18
Total			28

Integrated Gas Sampling Data:

Bag Pump No. 23 B
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check: 0
Time start: 1430
Sampling rate: 400

Box No. 22 Bag No. 3
Size: 44 L
cc/min at 14 in. Hg.
(HRS) Time end: 1527 (HRS)
cc/min Operator: DWH

S/N of O₂ Analyzer used to monitor train outlet:

24A

123093-GASTACKIWP\METHODS\0046RR

INTERPOL LABORATORIES EPA METHOD 5 FIELD DATA SHEET

Job L.P. Hayward Operator John D.M. Pitot No. 23-8 Cp 840
 Source Line 2 Press Vent RTO Stack Meter Box No. 6 Bar. Press. 28.90 inHg H2O
 Date 6/19/94 Gas meter const. 9947 Nozzle No. g152 Nozzle Dia. 246 in.

Traverse Point No.	Sampling Time (min)	Sample Volume (cf)	Velocity Head (inHg)	Drifts Water (inHg)	Des. Vol. (cf)	VAC. inHg	Temperature (°F)						Oxygen (Kv/v)
							Stack	Probe	Duct	Imp.	Gas/Dut		
A-12	(1425)	781.20											
	2.5	783.50	.88	2.78	3.50	8	253	241	260	45	87	85	20.6
	5	785.71	.85	2.68	5.77	7	252				93	85	20.5
	7.5	787.89	.77	2.44	7.94	7	254				96	85	20.6
	10	790.21	.91	2.90	0.31	8	250	245	258	47	98	85	20.6
	12.5	792.63	.90	2.86	2.66	9	253				100	86	20.5
	15	795.00	.93	2.94	5.05	9	260				101	86	20.5
	17.5	797.33	.86	2.73	7.35	8	258	248	261	48	103	87	20.5
	20	799.72	.96	3.06	9.79	8	256				104	88	20.5
	22.5	802.13	.95	3.04	2.23	9	254				104	88	20.6
3	25	804.40	.75	2.41	4.40	9	257	250	258	50	105	88	20.7
2	27.5	806.60	.78	2.50	6.62	8	254				106	89	20.7
1	30	808.79	.76	2.44	8.80	7	256				107	89	20.9
AB-12	32.5	810.98	.79	2.53	1.03	7	256	252	255	49	103	90	20.7
	35	813.17	.77	2.45	3.22	7	259				106	90	20.6
	37.5	815.46	.90	2.87	5.59	7	260				107	90	20.6
	40	817.91	.96	3.06	8.04	8	260	254	258	52	108	90	20.6
	42.5	820.40	.97	3.10	0.51	9	259				108	91	20.6
	45	822.92	1.03	3.30	3.05	10	257				108	91	20.6
	47.5	825.31	.83	2.66	5.34	9	259	258	257	51	109	91	20.6
	50	827.60	.81	2.63	7.61	8	249				109	91	20.6
	52.5	829.82	.77	2.47	9.82	8	257				109	91	20.5
	55	832.03	.79	2.52	2.05	7	261	251	254	50	110	92	20.5
2	57.5	834.15	.71	2.28	4.17	8	260				110	92	20.5
1	60	836.23	.69	2.22	6.26	7	259				110	92	20.6
(1527)													
θ = 60		V _h = 55.03	ΔH = 2.6								Avg. = 96.5		

INTERPOLL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job L.P. Hayward Date 6/9/94 Test 14 Run 3
Source Line 2 Press Vent PTD STACK No. of traverse points 24
Method 5 Filter holder: 7/955 Filter type: passiflex
Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
Post test: 0 cfm at 6 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

Recovery solvent(s)

☒ Acetone _____
☐ other(s) _____

No. of probe wash bottles:
Sample recovered by:

6
DVH

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1		200	
Impinger No. 2	209		9
Impinger No. 3			
Condenser			
Desiccant	1448	1435	13
Total			22

Integrated Gas Sampling Data:

Bag Pump No. 238
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check: 0
Time start: 1608
Sampling rate: 400

Box No. 22 Bag No. 3
Size: 44 L
cc/min at 14 in. Hg.
(HRS) Time end: 1719 (HRS)
cc/min Operator: DVH

S/N of O₂ Analyzer used to monitor train outlet:

24A

123093-G:\STACK\WP\METHODS\5-0046RR

Visible Emissions Form

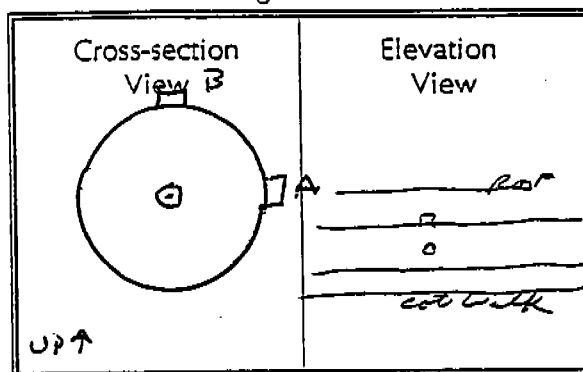
T14

SOURCE NAME <u>Louisiana Pacific</u>			OBSERVATION DATE <u>6-9-94</u>		START TIME <u>12:40</u>		STOP TIME <u>1:40</u>	
ADDRESS <u>RFD 8</u>			SEC MIN		SEC MIN			
			0 15 30 45		0 15 30 45			
			1 0 0 0 0		31 0 0 0 0			
			2 0 0 0 0		32 0 0 0 0			
CITY <u>Hayward</u> STATE <u>WI</u> ZIP <u>54843</u>			3 0 0 0 0		33 0 0 0 0			
PHONE			4 0 0 0 0		34 0 0 0 0			
SOURCE ID NUMBER			5 0 0 0 0		35 0 0 0 0			
PROCESS EQUIPMENT <u>Line 2 Press Stack</u>			OPERATING MODE <u>100%</u>		6 0 0 0 0		36 0 0 0 0	
CONTROL EQUIPMENT <u>RTO</u>			OPERATING MODE <u>100%</u>		7 0 0 0 0		37 0 0 0 0	
DESCRIBE EMISSION POINT <u>TALL Silver Stack near RR Tracks on North Side</u>			STOP <u>SAME</u>		8 0 0 0 0		38 0 0 0 0	
HEIGHT ABOVE GROUND LEVEL <u>START 400' STOP SAME</u>			HEIGHT RELATIVE TO OBSERVER <u>START 100' STOP SAME</u>		9 0 0 0 0		39 0 0 0 0	
DISTANCE FROM OBSERVER <u>START 500' STOP SAME</u>			DIRECTION FROM OBSERVER <u>START 315° STOP SAME</u>		10 0 0 0 0		40 0 0 0 0	
DESCRIBE EMISSIONS <u>START NONE STOP NONE</u>			11 0 0 0 0		41 0 0 0 0			
EMISSION COLOR <u>START None STOP SAME</u>			12 0 0 0 0		42 0 0 0 0			
PLUME TYPE: CONTINUOUS ☐ FUGITIVE ☐ INTERMITTENT ☐			13 0 0 0 0		43 0 0 0 0			
WATER DROPLETS PRESENT: NO ☒ YES ☐			14 0 0 0 0		44 0 0 0 0			
IF WATER DROPLET PLUME: ATTACHED ☐ DETACHED ☐			15 0 0 0 0		45 0 0 0 0			
POINT IN THE PLUME AT WHICH OPACITY WAS DETERMINED <u>START Directly above Stack Exit STOP SAME</u>			16 0 0 0 0		46 0 0 0 0			
DESCRIBE BACKGROUND <u>START Clear Sky STOP Broken Sky</u>			17 0 0 0 0		47 0 0 0 0			
BACKGROUND COLOR <u>START Blue STOP Blue/white</u>			18 0 0 0 0		48 0 0 0 0			
SKY CONDITIONS <u>START Clear STOP Broken</u>			19 0 0 0 0		49 0 0 0 0			
WIND SPEED <u>START 5mph STOP 10mph</u>			20 0 0 0 0		50 0 0 0 0			
WIND DIRECTION <u>START SW STOP SAME</u>			21 0 0 0 0		51 0 0 0 0			
WET BULB TEMP. <u>62</u> RH. percent <u>71%</u>			22 0 0 0 0		52 0 0 0 0			
AMBIENT TEMP. <u>70</u> STOP <u>SAME</u>			23 0 0 0 0		53 0 0 0 0			
			24 0 0 0 0		54 0 0 0 0			
			25 0 0 0 0		55 0 0 0 0			
			26 0 0 0 0		56 0 0 0 0			
			27 0 0 0 0		57 0 0 0 0			
			28 0 0 0 0		58 0 0 0 0			
			29 0 0 0 0		59 0 0 0 0			
			30 0 0 0 0		60 0 0 0 0			
			AVERAGE OPACITY FOR HIGHEST PERIOD			NUMBER OF READINGS ABOVE % WERE		
RANGE OF OPACITY READINGS MINIMUM 0 MAXIMUM 0								
OBSERVER'S NAME (PRINT) <u>Edward Jurs III</u>			DATE <u>6-9-94</u>					
OBSERVER'S SIGNATURE <u>[Signature]</u>								
ORGANIZATION <u>Interpoll Labs Inc.</u>								
I HAVE RECEIVED A COPY OF THESE OPACITY OBSERVATIONS SIGNATURE			CERTIFIED BY <u>Eastern Technical Assoc.</u>			DATE <u>4-6-94</u>		
TITLE			DATE			VERIFIED BY		
						DATE		

EPA Method 2 Field Data Sheet

Drawing of Test Site

Job LP - HAYWARD
Source E2 PRESS RTD INLET
Test 21 Run 0 Date 6-8-94 + 6-9-94
Stack Dimen. 58.5 IN.
Dry Bulb 110 °F Wet bulb _____ °F
Manometer ☒ Reg. ☐ Exp ☐ Elec.
Barometric Pressure 28.90 IN.HG
Static Pressure -4.40 IN.WC
Operators SB + KN
Pitor No. 025-6 C. .840

[illegible]

R or nothing = reg. manometer; S = expanded; E = electronic

INTERPOLL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job LD - HAYWARD
Source #2 PROS. RTD INLET
Method 1-5 Filter holder: TEFLON
Sample Train Leak Check:

Date 6-9-94 Test 21 Run - 1
No. of traverse points 12
Filter type: 3.5" Pallflex

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
Post test: 0.00 cfm at 12 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

1315

Recovery solvent(s)

☒ acetone _____
☐ other(s) _____

No. of probe wash bottles:

1
SD

Sample recovered by:

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2	<u>504</u>	<u>502</u>	<u>2</u>
Impinger No. 3			
Condenser			
Desiccant	<u>1500</u>	<u>1478</u>	<u>22</u>
Total			<u>24</u>

Integrated Gas Sampling Data:

(ambient air)

Bag Pump No. _____
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check: _____
Time start: _____
Sampling rate: _____

Box No. _____ Bag No. _____
Size: 44 L
cc/min at _____ in. Hg.
(HRS) Time end: _____ (HRS)
cc/min Operator: _____

S/N of O₂ Analyzer used to monitor train outlet: _____

123093-GASTACKWPMETHODS-0046RR

041

1

[illegible][illegible]

INTERPOLL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job LP-HAYWARD Date 6-9-94 Test 21 Run 2
Source #2 PUMP RD FULLER No. of traverse points 12
Method 1-5 Filter holder: TEFLON Filter type: 3.52" DMPLEX
Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
Post test: 0.00 cfm at 18 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

1316

Recovery solvent(s)

☒ Acetone _____
☐ other(s) _____

No. of probe wash bottles:

Sample recovered by:

SB
SB + ES + KN

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2	<u>301</u>	<u>500</u>	<u>1</u>
Impinger No. 3			
Condenser			
Desiccant	<u>1549</u>	<u>1526</u>	<u>23</u>
Total			<u>24</u>

Integrated Gas Sampling Data:

(Ambient air)

Bag Pump No. _____
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check: _____
Time start: _____
Sampling rate: _____

Box No. _____ Bag No. _____
Size: 44 L
cc/min at _____ in. Hg.
(HRS) Time end: _____ (HRS)
cc/min Operator: _____

S/N of O₂ Analyzer used to monitor train outlet: _____

123093-G:\STACK\WP\METHODS\S-0046RR

INTERPOL LABORATORIES EPA METHOD 5 FIELD DATA SHEET

1000	LP- 44444444	Operator	3D+K4	Printer No.	220-6	Cp	840
1001	42 press	Model Box No.	14	Printer No.	3830	10119	120 3
1002	6-9-94	Generator Code	10066	Model No.	4-3	10114	122 11
1003	12	Rev	2				

Traverse Point No.	Sampling Time (min)	Sample Volume (cf)	Velocity Head (ft)	Drifts Meter (ft)	Dye Vol (cf)	VAD. inHg	Temperature (°F)					Gas/Det	Oxygen (xv/v)
							Stack	Probe	Dye	Temp.	Gas In		
B-6	(1725)	1058.83	1.50	1.41	217	6	124	247	251	47	82	81	20.9
	5	1062.10	1.50	1.43	5.54	8	119	247	254	46	92	87	Anal.
	10	1065.59	1.56	1.49	8.99	8	120	247	254	46	79	81	air
	15	1068.98	2.60	2.57	3.48	10	120	247	254	46	102	82	
	20	1073.62	2.75	2.66	8.11	12	120	247	254	46	103	83	
	25	1078.30	2.50	2.42	5.53	11	121	247	255	45	104	83	
A-6	30	1082.64	2.50	2.43	6.95	12	121	247	256	45	104	83	
	35	1086.90	2.45	2.38	1.33	10	121	248	257	45	102	87	
	40	1091.30	2.35	2.28	5.63	10	123	250	257	40	105	88	
	45	1095.60	2.45	2.37	0.03	10	121	249	256	40	106	89	
	50	1100.00	2.30	2.25	4.31	10	120	251	254	41	107	90	
	55	1104.50	2.50	2.45	8.78	10	120	250	254	41	108	91	
	60	1108.78											
	(1530)												
Σ = 60		Σ = 49.93		Σ = 2.07								Avg. = 92.0	

INTERPOLL LABORATORIES EPA METHOD 5/17 SAMPLE LOG SHEET

Job LP- HAYWARD
 Source #2 PRESS MTD INLET
 Method 1-5 Filter holder: 746L02

Date 6-9-94 Test 21 Run 3
 No. of traverse points 12
 Filter type: 3.52" PALFLEX

Sample Train Leak Check:

Pretest: { 0.02 cfm at 15 in. Hg. (vac) ☒
 Posttest: 0.00 cfm at 14 in. Hg. (vac) ☒

Particulate Catch Data:

No.s of filters used: 1317 Recovery solvent(s)
☒ acetone
☐ other(s) _____
 No. of probe wash bottles: 1
 Sample recovered by: SD + KN + ET

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2	<u>502</u>	<u>500</u>	<u>2</u>
Impinger No. 3			
Condenser			
Desiccant	<u>1555</u>	<u>1530</u>	<u>25</u>
Total			<u>27</u>

Integrated Gas Sampling Data: (Ambient Air)

Bag Pump No. _____ Box No. _____ Bag No. _____
 Bag Material: 5-layer Aluminized Tedlar Size: 44 L
 Pretest leak check: _____ cc/min at _____ in. Hg.
 Time start: _____ (HRS) Time end: _____ (HRS)
 Sampling rate: _____ cc/min Operator: _____
 S/N of O₂ Analyzer used to monitor train outlet: _____

CF-023

Lab	LP- MAYWARD	Operators	SB+KN	Pilot No.	220-6	Cp	220
Source	22 Dec 51	Water Box No.	14	Bar. Press.	28.80	10Hg	H2O 3
Unit	3-9-51	Generator Count.	1,006	Nozzle No.	7-3	NOZZLE DIA.	1.72 IN.

[illegible]

VISIBLE EMISSIONS EVALUATOR

This is to certify that

David Wheeler

met the specifications of Federal Reference Method 9 and qualified as a visible emissions evaluator. Maximum deviation on white and black smoke did not exceed 7.5% opacity and no single error exceeding 15% opacity was incurred during the certification test conducted by Eastern Technical Associates of Raleigh, North Carolina. This certificate is valid for six months from date of issue.

Thomas Lane
President

Will Savage, Jr.
Vice President

David B. Savage, Jr.
Program Manager

243003
Certificate Number

Minneapolis
Location

April 6, 1994
Date of Issue

VISIBLE EMISSIONS EVALUATOR

This is to certify that

Edward J. Gaud

met the specifications of Federal Reference Method 9 and qualified as a visible emissions evaluator. Maximum deviation on white and black smoke did not exceed 7.5% opacity and no single error exceeding 15% opacity was incurred during the certification test conducted by Eastern Technical Associates of Raleigh, North Carolina. This certificate is valid for six months from date of issue.

Thermon Hare
President

Will Savage, Jr.
Vice President

David B. Savage, Jr.
Program Manager

243004
Certificate Number

Minneapolis
Location

April 6, 1994
Date of Issue

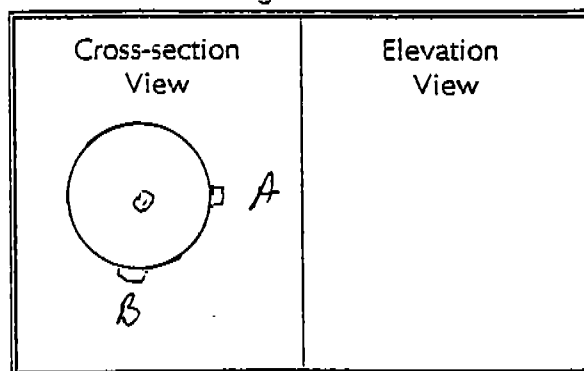
APPENDIX D

KONUS FIELD DATA SHEETS

EPA Method 2 Field Data Sheet

Drawing of Test Site

Job 211 HAYWARD
Source LINE 1 KONUS STACK
Test 5 Run 0 Date 6-8-94
Stack Dimen. 32.0 IN.
Dry Bulb °F Wet bulb °F
Manometer ☒ Reg. ☐ Exp. ☐ Elec.
Barometric Pressure 28.45 IN.HG
Static Pressure -.20 IN.WC
Operators E.T. ROWBRIDGE - D. Walker
Pitot No. 24V-5 C. .840



Traverse Point No.	Fraction of Diameter	Distance From Stack Wall (IN.)	Distance From End of Port (IN.)	Velocity	Temp. of Gas (°F)
Port Length: 6.5 IN.		Time Start: 0820 HRS			
A 1	.026	1.35	7.85	.11	
2	.082	4.26	10.86	.13	
3	.146	7.69	14.09	.13	
4	.226	11.89	18.29	.13	
5	.342	17.98	24.38	.12	325
6	.658	34.22	40.72	.12	
7	.774	40.24	46.74	.11	
8	.954	44.80	50.90	.12	
9	.918	48.74	54.24	.11	
10	.974	50.64	57.04	.08	
B 1				.09	
2				.10	
3				.11	
4				.11	327
5				.11	
6				.12	
7				.13	
8				.13	
9				.14	
10				.15	
Temp. Meas. Device & S/N: PTT-34				Time End: 0812 HRS	

R or nothing = reg. manometer; S = expanded; E = electronic

032594-G:STACK\WP\FORMS\S-392.1

INTERPOL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job LP/HAYWARD Date 6-8-94 Test 5 Run 1
Source LINE 1 KANUS STACK No. of traverse points 20
Method 5 Filter holder: 414055 Filter type: 4" PALLFLAX
Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
Post test: 0 cfm at 6 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

4031

Recovery solvent(s)

☒ Acetone _____
☐ Other(s) _____

No. of probe wash bottles:

1

Sample recovered by:

ET

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1		<u>100</u>	
Impinger No. 2	<u>257</u>	<u>100</u>	<u>57</u>
Impinger No. 3		<u>0</u>	
Condenser			
Desiccant	<u>1363</u>	<u>1350</u>	<u>13</u>
Total			<u>70</u>

Integrated Gas Sampling Data:

Bag Pump No. 248
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check: 0
Time start: 1539
Sampling rate: 400

Box No. 17 Bag No. 1
Size: 44 L
cc/min at 1.5 in. Hg.
(HRS) Time end: 1639 (HRS)
cc/min Operator: ET

S/N of O₂ Analyzer used to monitor train outlet:

248

123093-G:\STACK\WPMETHODS\0046RR

LP/HAYWARD
5/20/85
6-8-85

J 1 4 7 9
x 8 9
B 1 4 7 9

E7-DV
x 1.77 = 9036

Pital No. 244-5-
Bor. Price. 28.00
Kozilya No. 1-1/2

By 1009 HZ
Hoxly Din

840

[illegible]

INTERPOL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job LP/HAYWARD Date 6-8-94 Test 5 Run 2
Source LIAR 1 HONUS STACK No. of traverse points 20
Method 5 Filter holder: 4" GLASS Filter type: 4" PALL FLAX
Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
Post test: 0 cfm at 6 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

4032

Recovery solvent(s)

☒ Acetone _____
☐ Other(s) _____

No. of probe wash bottles:

Sample recovered by:

1
ET

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1		(100)	
Impinger No. 2	251	100	51
Impinger No. 3		0	
Condenser			
Desiccant	1434	1423	11
Total			62

Integrated Gas Sampling Data:

Bag Pump No. 248
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check: 0
Time start: 1709
Sampling rate: 400

Box No. 17 Bag No. 2
Size: 44 L
cc/min at 15 in. Hg.
(HRS) Time end: 1810 (HRS)
cc/min Operator: ET

S/N of O₂ Analyzer used to monitor train outlet:

248

INTERPOL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job LP/HAYWARD Date 10-8-94 Test 5 Run 3
Source LINOI KODAKS STACK No. of traverse points 20
Method 5 Filter holder: 4" GLASS Filter type: 4" Pall Flt
Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
Post test: 0 cfm at 6 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

4033

Recovery solvent(s)

☒ Acetone
☐ Other(s)

No. of probe wash bottles:

Sample recovered by:

1
ET

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1		(120)	
Impinger No. 2	271	100	71
Impinger No. 3		0	
Condenser			
Desiccant	1375	1365	10
Total			81

Integrated Gas Sampling Data:

Bag Pump No. 24B
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check: 0
Time start: 1836
Sampling rate: 400

Box No. 17 Bag No. 3
Size: 44 L
cc/min at 15 in. Hg.
(HRS) Time end: 1937 (HRS)
cc/min Operator: ET

S/N of O₂ Analyzer used to monitor train outlet:

24B

Interpoll Laboratories
(612)786-6020

EPA Method 7 Sample Collection
Field Data Sheet

Job L.P. Hays Date 6-8-94 Bar. Pressure 28.90 IN.HG.
Test Location STACK Fuel Type BARK Sample Train No. 3062
Line 1 KORVS Technician D.J. Pump No. 24A

No.	Test Run Point	Flask No.	Time (HRS)	Vacuum (IN.HG.)	Flask Temp. (°F)	Leak Rate < 0.4 IN.HG./MIN.	
1	5-1-1	19	1540	27.33	70	☒ Yes	☐ No
2	5-1-1	20	1552	27.35	70	☒ Yes	☐ No
3	5-1-1	21	1604	27.41	70	☒ Yes	☐ No
4	5-1-1	22	1632	27.40	70	☒ Yes	☐ No
5	5-2-1	23	1708	27.39	70	☒ Yes	☐ No
6	5-2-1	24	1723	27.28	70	☒ Yes	☐ No
7	5-2-1	61	1738	27.58	70	☒ Yes	☐ No
8	5-2-1	62	1755	27.44	70	☒ Yes	☐ No
9	5-3-1	63	1835	27.47	70	☒ Yes	☐ No
10	5-3-1	64	1850	27.40	70	☒ Yes	☐ No
11	5-3-1	65	1910	27.44	70	☒ Yes	☐ No
12	5-3-1	66	1925	27.53	70	☒ Yes	☐ No
13						☐ Yes	☐ No
14						☐ Yes	☐ No
15						☐ Yes	☐ No
16						☐ Yes	☐ No
17						☐ Yes	☐ No
18						☐ Yes	☐ No
19						☐ Yes	☐ No
20						☐ Yes	☐ No
21						☐ Yes	☐ No
22						☐ Yes	☐ No
23						☐ Yes	☐ No
24						☐ Yes	☐ No
25						☐ Yes	☐ No
26						☐ Yes	☐ No
27						☐ Yes	☐ No

Interpoll Laboratories
(612)786-6020

Visible Emissions Form

T5

SOURCE NAME <u>Louisiana Pacific</u>		OBSERVATION DATE <u>6-8-94</u>		START TIME <u>15:38</u>		STOP TIME <u>16:38</u>					
ADDRESS		SEC MIN	0	15	30	45	SEC MIN	0	15	30	45
		1	0	0	0	0	31	0	0	0	0
CITY <u>Hayward</u>	STATE <u>WI</u>	ZIP	2	0	0	0	32	0	0	0	0
PHONE	SOURCE ID NUMBER		3	0	0	0	33	0	0	0	0
		4	0	0	0	0	34	0	0	0	0
PROCESS EQUIPMENT <u>Konus-Line 1</u>		OPERATING MODE <u>100%</u>		5	0	0	0	35	0	0	0
CONTROL EQUIPMENT <u>EFB</u>		OPERATING MODE <u>100%</u>		6	0	0	0	36	0	0	0
DESCRIBE EMISSION POINT <u>Short Gray Stack on South East Side of Building</u>		SAME		7	0	0	0	37	0	0	0
HEIGHT ABOVE GROUND LEVEL START ~72' STOP SAME		HEIGHT RELATIVE TO OBSERVER START ~72' STOP SAME		8	0	0	0	38	0	0	0
DISTANCE FROM OBSERVER START ~300' STOP SAME		DIRECTION FROM OBSERVER START ~355° STOP SAME		9	0	0	0	39	0	0	0
				10	0	0	0	40	0	0	0
DESCRIBE EMISSIONS START NONE STOP SAME				11	0	0	0	41	0	0	0
EMISSION COLOR START NONE STOP SAME		PLUME TYPE: CONTINUOUS ☐ FUGITIVE ☐ INTERMITTENT ☐		12	0	0	0	42	0	0	0
WATER DROPLETS PRESENT: NO ☒ YES ☐		IF WATER DROPLET PLUME: ATTACHED ☐ DETACHED ☐		13	0	0	0	43	0	0	0
POINT IN THE PLUME AT WHICH OPACITY WAS DETERMINED START Directly Above Stack Exit STOP SAME				14	0	0	0	44	0	0	0
DESCRIBE BACKGROUND START Blue Sky STOP SAME				15	0	0	0	45	0	0	0
BACKGROUND COLOR START Blue Sky STOP SAME		SKY CONDITIONS START Clear STOP SAME		16	0	0	0	46	0	0	0
WIND SPEED START 15 mph STOP SAME		WIND DIRECTION START NW STOP SAME		17	0	0	0	47	0	0	0
AMBIENT TEMP. START 72° STOP SAME		WET BULB TEMP. 63°		18	0	0	0	48	0	0	0
		RH. percent 72%		19	0	0	0	49	0	0	0
Source Layout Sketch (1/4 mi) Draw North Arrow Stack Emission Point Observers Position Sun Location Line Wind Plume and Stack 40° Wood Piles		20	0	0	0	50	0	0	0	0	
		21	0	0	0	51	0	0	0	0	
		22	0	0	0	52	0	0	0	0	
		23	0	0	0	53	0	0	0	0	
		24	0	0	0	54	0	0	0	0	
		25	0	0	0	55	0	0	0	0	
		26	0	0	0	56	0	0	0	0	
		27	0	0	0	57	0	0	0	0	
		28	0	0	0	58	0	0	0	0	
		29	0	0	0	59	0	0	0	0	
		30	0	0	0	60	0	0	0	0	
		AVERAGE OPACITY FOR HIGHEST PERIOD		NUMBER OF READINGS ABOVE % WERE		RANGE OF OPACITY READINGS		MINIMUM		MAXIMUM	
OBSERVER'S NAME (PRINT) <u>Edward J. Jers III</u>		OBSERVER'S SIGNATURE <u>[Signature]</u>		DATE <u>6-8-94</u>		ORGANIZATION <u>Interpoll Labs, Inc.</u>					
COMMENTS		I HAVE RECEIVED A COPY OF THESE OPACITY OBSERVATIONS SIGNATURE		CERTIFIED BY <u>Eastern Tech. Assoc.</u>		DATE <u>4-6-94</u>					
TITLE		DATE		VERIFIED BY		DATE					

INTERPOL LABORATORIES, INC.
(612) 786-6020
EPA Method 2 Field Data Sheet

Drawing of Test Site

Job 281 HAYWARD
Source LINE 1 KANUS
Test 6 Run Date 6-4-84
Stack Dimen. 52 IN.
Dry Bulb °F Wet bulb °F
Manometer ☒ Reg. ☐ Exp ☐ Elec.
Barometric Pressure 28.90 IN.HG
Static Pressure -1.20 IN.WC
Operators E. Trowbridge - R. Rosenthal
Pitot No. 24V-5 C. 1840

Cross-section
View

Elevation
View

[illegible]

R or nothing = reg. manometer; S = expanded; E = electronic

032594-G:STACKIWPIFORMSIS-392.1

INTERPOLL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job LP/HAYWARD Date 6-9-94 Test 6 Run 1
Source LINCOLN RADIUS STACK No. of traverse points 20
Method SO₂/1 Filter holder: N/A Filter type: NA
Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
Post test: 0 cfm at 13 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

NA

Recovery solvent(s)

☐ acetone
☒ Other(s) MC

No. of probe wash bottles:

Sample recovered by:

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1		<u>100</u>	
Impinger No. 2	<u>268</u>	<u>100</u>	<u>68</u>
Impinger No. 3		<u>0</u>	
Condenser			
Desiccant	<u>1522</u>	<u>1506</u>	<u>16</u>
Total			<u>84</u>

Integrated Gas Sampling Data:

Bag Pump No. 2413
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check: 0
Time start: _____
Sampling rate: 400

Box No. 17 Bag No. 1
Size: 44 L
cc/min at 15 in. Hg.
(HRS) Time end: _____ (HRS)
cc/min Operator: RT

S/N of O₂ Analyzer used to monitor train outlet:

248

1000 28/HAYWARD
50000 LINE 1 KOREA
10000 6-9-92

100 L P HAYWARD
EQUIVA LINE 1 KANSAS STATE
Only 6-9-94 1001 6 NOV 1

Dep't of Justice
 Bureau of Prisons
 Washington, D.C.

ET-XR
2 111 127 111 127 111 127

P. 111
 P. 112
 P. 113

7-18

[illegible]

INTERPOLL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job LP/HAYWARD Date 6-9-84 Test 6 Run 2
Source LINDI KONUS STACK No. of traverse points 20
Method SOIL Filter holder: NA Filter type: NA
Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
Post test: 0 cfm at 13 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

NA

Recovery solvent(s)

☐ acetone
☒ other(s) MC

No. of probe wash bottles:

Sample recovered by:

1
ET

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1		<u>100</u>	
Impinger No. 2		<u>100</u>	<u>94</u>
Impinger No. 3		<u>0</u>	
Condenser			
Desiccant	<u>1533</u>	<u>1522</u>	<u>11</u>
Total			<u>105</u>

Integrated Gas Sampling Data:

Bag Pump No. 248
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check: 0
Time start: 1633
Sampling rate: 400

Box No. 17 Bag No. 2
Size: 44 L
cc/min at 15 in. Hg.
(HRS) Time end: 1742 (HRS)
cc/min Operator: ET

S/N of O₂ Analyzer used to monitor train outlet:

248

CP/HAYWARD
CINCO: ROM
4-3-91

[illegible]

ET-58
2 117 1.9974

Put the
Bar. Pin
Hole in

5/25/43

[illegible]

INTERPOLL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job LP/HAYWARD
Source LINE 1 KANUS STACK
Method SO₂ Filter holder: NA
Sample Train Leak Check:

Date 6-9-44 Test 6 Run 3
No. of traverse points 20
Filter type: NA

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ✓
Post test: 0 cfm at 15 in. Hg. (vac) ✓

Particulate Catch Data:

No. of filters used:

NA

Recovery solvent(s)

☐ acetone
☒ other(s) MC

No. of probe wash bottles:

Sample recovered by:

1
ET

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1		{ 100 }	
Impinger No. 2	294	{ 100 }	74
Impinger No. 3		{ 0 }	
Condenser			
Desiccant	1440	1425	15
Total			94

Integrated Gas Sampling Data:

Bag Pump No. 24B
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check: 0
Time start: 1803
Sampling rate: 400

Box No. 17 Bag No. 3
Size: 44 L
cc/min at 15 in. Hg.
(HRS) Time end: 1903 (HRS)
cc/min Operator: ET

S/N of O₂ Analyzer used to monitor train outlet:

24B

Drawing of Test Site

Cross-section View	Elevation View
-----------------------	-------------------

Phenol

[illegible]

032594G:STACK\WP\FORMS\5-392.1

INTERCOLL LABORATORIES
EPA Method 4 and 6 Field Data Sheet

Job LPI/HANNUAL
Source LINE 1 KANUS STAIR
Date 6-9-84 Test 7 Run 1

Operator(s) E. TRUMBULL & ROSENTHAL
Meter Box No. 2 Gas meter coef. 9974
 ΔH 1.77 in. WC Bar. press 28.90 in. Hg

Sample Train Leak Check:

Pretest: < 0.02 cfm at 15 in. Hg.

Posttest: 0 cfm at 17 in. Hg.

☒ ☐

Trav. Point No.	Samp. Time (min)	Sample Volume (cf)	Drift. Meter (inWC)	VAC. inHg	Temperatures (°F)					Oxygen
					Probe	Oven	Impg.	Gas/In	Gas/Out	(%v/v)
	0845	893.60								
1	5	897.40	1.77	10	245	250	43	68	62	15.9
1	10	901.20	1.77	9.8	248	252	45	73	63	15.7
1	15	904.95	1.77	9.8	251	255	45	74	63	16.0
1	20	908.70	1.77	9.8	250	256	47	75	64	15.7
2	25	912.46	1.77	9.8	230	244	40	76	65	15.2
2	30	916.25	1.77	9.8	235	248	40	78	66	15.0
2	35	919.95	1.77	9.8	242	251	42	80	67	14.7
2	40	923.66	1.77	9.8	245	250	42	80	67	14.5
3	45	927.40	1.77	9.8	242	253	42	81	68	14.4
3	50	931.12	1.77	9.8	240	251	42	83	69	14.3
3	55	934.90	1.77	9.8	240	255	42	85	70	14.8
3	60	938.80	1.77	9.8	257	249	42	86	72	14.3
	(0845)									
	$\theta = 60$	$V_m = 45.20$	$(\Delta H)_{avg} = 1.77$					$(t_m)_{avg} = 72.3$		

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impingers	254	200	54
Condenser			
Desiccant	1441	1429	12
Total			66

Preliminary results of SO ₂ concentration determination	
V_{std}	= 43.39 DSCF
Moisture	= 6.69 %v/v
SO ₂ , dry	= ppm
SO ₂ , wet	= ppm
LB/MMBtu	=

INTERPOL LABORATORIES
EPA Method 4 and 6 Field Data Sheet

Job CP/HAYWARD
Source Unit 1 Marine Stack
Date 6-4-84 Test 7 Run 2

Operator(s) ET-KR
Meter Box No. 2 Gasmeter coef. 9974
 $\bar{V}_H$ 1.77 in.WC Bar. press 29.94 in.Hg

Sample Train Leak Check:

Pretest: < 0.02 cfm at 15 in. Hg.
Posttest: 0 cfm at 10 in. Hg.

Trav. Point No.	Samp. Time (min)	Sample Volume (cf)	Orif. Meter (inWC)	VAC. inHg	Temperatures (°F)					Oxygen (%v/v)
					Probe	Oven	Impg.	Gas/In	Gas/Out	
	1000	939.20								
	5	943.00	1.77	9.8	245	251	39	79	73	14.2
	10	946.70	1.77	9.8	251	255	40	79	73	15.1
	15	950.45	1.77	9.8	250	252	40	79	73	14.5
	20	954.30	1.77	9.8	252	254	40	79	74	14.5
	25	958.10	1.77	9.8	250	251	41	79	74	15.0
	30	961.94	1.77	9.8	254	252	41	79	74	15.4
	35	965.80	1.77	9.8	250	254	42	79	74	16.0
	40	969.65	1.77	9.8	250	253	42	79	74	14.7
	45	973.40	1.77	9.8	261	263	48	80	75	16.1
	50	977.21	1.77	10	260	261	48	81	75	16.8
	55	981.02	1.77	10	262	260	48	82	75	16.4
	60	984.83	1.77	10	260	258	48	82	75	16.1
	(1100)									
	$\theta = 60$	$V_m = 45.63$	$(\bar{V}_H)_{avg} = 1.77$					$(t_m)_{avg} = 76.9$		

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impingers	261	200	61
Condenser			
Desiccant	1506	1495	11
	Total		72

Preliminary results of SO ₂ concentration determination	
V_{std}	= 43.43 DSCF
Moisture	= 7.24 %v/v
SO ₂ , dry	= ppm
SO ₂ , wet	= ppm
LB/MMBtu	=

INTERPOL LABORATORIES
EPA Method 4 and 6 Field Data Sheet

Job LP/HAYWARD
Source LINCOLN ROUNDS STACK
Date 6-9-94 Test 7 Run 3

Operator(s) ET-KR
Meter Box No. 2 Gasmeter coef. 1.9974
 ΔH 1.77 in.WC Bar. press 28.50 in.Hg

Sample Train Leak Check:

Pretest: < 0.02 cfm at 15 in. Hg. ☒
Posttest: 0 cfm at 12 in. Hg. ☒

Trav. Point No.	Samp. Time (min)	Sample Volume (cf)	Drift Meter (inWC)	VAC. inHg	Temperatures (°F)					Oxygen (%v/v)
					Probe	Oven	Impg.	Gas/In	Gas/Out	
	11/1	985.30								
1	5	989.22	1.77	10	247	258	42	81	75	14.5
1	10	993.25	1.77	10	252	260	42	83	75	16.0
1	15	996.90	1.77	10	255	261	44	83	75	16.0
1	20	1000.87	1.77	10	256	260	44	84	75	17.0
2	25	1004.66	1.77	10	252	261	40	76	74	15.0
2	30	1008.50	1.77	10	255	258	42	78	74	15.0
2	35	1012.10	1.77	10	257	260	44	81	74	16.2
2	40	1015.99	1.77	10	259	258	44	83	74	15.6
3	45	1019.77	1.77	10	262	256	45	85	76	14.9
3	50	1023.45	1.77	10	260	258	46	87	77	15.4
3	55	1027.80	1.77	10	256	260	46	88	77	15.3
3	60	1030.80	1.77	10	250	254	46	89	78	15.7
	(1320)									
	0=60	$V_m = 45.50$	(ΔH) = 1.77					$(t_m)_{avg} = 79.1$		

1129
6.10.94
in. Hg

Condensate Data:

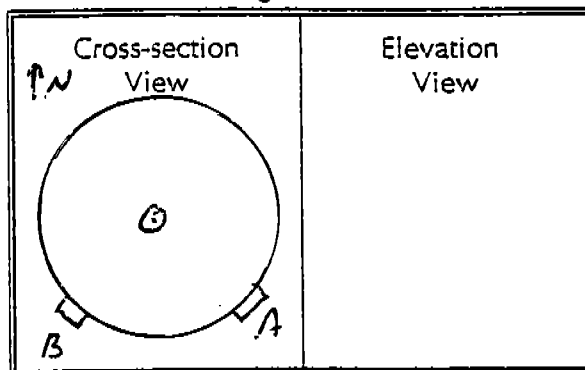
Item	Weight (g)		
	Final	Tare	Difference
Impingers	253	200	53
Condenser			
Desiccant	1415	1390	25
Total			78

Preliminary results of SO ₂ concentration determination	
V _{std}	= 43.13 DSCF
Moisture	= 7.85 %v/v
SO ₂ , dry	= ppm
SO ₂ , wet	= ppm
LB/MMBtu	=

INTERPOL LABORATORIES, INC.
(612) 786-6020
EPA Method 2 Field Data Sheet

Drawing of Test Site

Job L.P. / Hayward, WI
Source Line 1 Keros / Stack
Test B Run 0 Date 6-9-94
Stack Dimen. 52.0 IN.
Dry Bulb 330 °F Wet bulb 134 °F
Manometer ☐ Reg. ☒ Exp ☐ Elec.
Barometric Pressure 28.90 IN.HG
Static Pressure -.20 IN.WC
Operators M. Kachler & K. Rosenblatt
Pitor No. MMS-6 C_p .84



Traverse Point No.	Fraction of Diameter	Distance From Stack Wall (IN.)	Distance From End of Port (IN.)	Velocity	Temp. of Gas (°F)
		Port Length: <u>6.5</u> IN.	Time Start: <u>0930</u> HRS		
A-1	.04	1.09	7.59	.060	
2	.067	3.48	9.98	.063	
3	.118	6.14	12.64	.075	
4	.177	9.20	15.70	.095	
5	.250	13.00	19.50	.090	
6	.356	18.51	25.01	.095	
7	.644	33.49	39.99	.102	
8	.750	39.00	45.50	.112	
9	.823	42.90	49.30	.120	
10	.992	45.86	52.36	.130	
11	.933	48.52	55.02	.125	
12	.979	50.91	57.41	.122	
B-1				.063	
2				.068	
3				.075	
4				.082	
5				.085	
6				.093	
7				.090	
8				.095	
9				.100	
10				.095	
11				.093	
12				.098	
Temp. Meas. Device & S/N: <u>PDT-31 / TC</u>				Time End: <u>0838</u> HRS	

R or nothing = reg. manometer; S = expanded; E = electronic

INTERPOLL LABORATORIES EPA MODIFIED METHOD 5 SAMPLE LOG SHEET

Job L.P. / Hayward, WI
 Source Line 1 Korus / Stuck
 Cyclone: ☐ Yes ☒ No Filter holder: MMS
 Analytes: POM
 Field recovery spike added: ☒ Yes ☐ No

Date 6-9-94 Test 8 Run 1
 No. of traverse points 24
 Filter type: 4" Glass fiber
 XAD-2 resin: g Batch No.
 Reference: EPA SW-846 Method 0010

Sample Train Leak Check:

Pretest: 0.02 cfm at 15 in. Hg. (vac) ☒
 Posttest: 20.02 cfm at 13 in. Hg. (vac) ☒

Semivolatile Catch Data:

No.s of filters used: 0347 Recovery solvent(s)
☒ MeCl₂ ☒ MeOH (50:50 v/v)
☒ other(s) Acetone

No. of bottles for condensate trap catch: 1
 Samples recovered by: Mike Schuler + K. Rausenthall

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Condensate trap			
Condensate trap	<u>133</u>	<u>0</u>	<u>133</u>
Condensate trap			
Impingers			
Desiccant	<u>1474</u>	<u>1448</u>	<u>26</u>
Total			<u>159</u>

Integrated Gas Sampling Data:

Bag Pump No. 294 Box No. 27 Bag No. 1
 Bag Material: 4-layer Aluminized Tedlar Size: 44 L
 Pretest leak check: 0 cc/min at 20 in. Hg.
 Time start: 0851 (HRS) Time end: 1052 (HRS)
 Sampling rate: 200 cc/min O₂ Analyzer S/N: 9

INTERPOL LABORATORIES EPA METHOD 1631 FIELD DATA SHEET

Job L.P. / Hymnwood, Cal. Operator M. Kneibler & K. Karsanthal Nozzle No. 415-7 Pitot No. 5-6
 Source Line 1, Reus 15, 15, 15 Water Box No. 9 Nozzle Dia. 1/222 In. Cp 94
 Date 8-9-94 Test 8 Run 1 Gasometer Const. 9961 Bar. Pres. 28.80 In. Hg H₂O 9 %

Traverse Point No.	Sampling Time (min)	Sample Volume (cc)	Velocity Head (in Hg)	Orifice Meter (in Hg)	Deg. Vol. (cc)	VAC. (in Hg)	Temperature (°F)					Oxygen	
							Stack	Probe	Open	XAD2	Imp.	Water (in/out)	(%v/v)
B-12	0851	677.20	.105	1.95	1.17	7.5	335	243	255	43	41	61	15.4
	5	681.21	.105	1.62	9.79	7	336	247	252	43	41	61	15.3
	10	684.85	.107	1.77	8.59	7	335	250	256	43	42	70	15.6
	15	688.57	.109	1.88	8.51	8	335	252	255	43	42	71	14.7
	20	692.48	.110	1.80	6.36	8	335	255	253	43	42	76	14.8
	25	696.31	.109	1.62	0.02	7	336	250	253	44	42	78	15.5
	30	700.06	.108	1.62	3.69	7	331	248	263	44	42	79	16.6
	35	703.74	.108	1.62	7.61	8	332	245	260	44	42	80	16.4
	40	707.70	.109	1.63	1.29	7	332	245	264	45	42	82	16.5
	45	711.37	.108	1.27	4.55	6	334	247	260	45	43	93	16.6
	50	714.63	.106	1.25	7.78	6	335	250	257	44	43	85	16.8
	55	717.95	.106	1.20	0.96	6	333	255	258	44	43	85	16.5
	60	720.98	.106	2.13	5.19	10	334	258	255	45	43	87	16.3
A-12	65	725.24	.110	2.40	9.68	11	335	254	259	44	43	87	16.4
	70	729.25	.124	2.49	4.26	11	332	251	263	44	44	87	16.4
	75	734.31	.128	2.23	8.59	10.5	334	255	260	44	44	87	15.2
	80	738.65	.115	2.19	2.90	10	327	254	263	46	44	88	15.5
	85	742.92	.112	2.00	7.01	9	327	250	264	46	44	88	15.3
	90	747.11	.102	1.72	0.93	8	329	247	261	46	44	89	15.6
	95	750.87	.108	1.31	4.17	6.5	328	245	261	46	44	89	14.4
	100	754.22	.106	1.24	7.41	6	328	248	256	47	45	90	16.0
	105	757.48	.106	1.48	0.96	7	325	246	249	45	43	91	15.7
	110	760.94	.107	1.13	4.06	5.5	324	245	252	45	43	91	16.8
	115	764.15	.105	1.09	7.11	5.5	324	242	250	45	44	92	16.8
	120	767.14	.105	1.09	7.11	5.5	324	242	250	45	44	92	16.8
	(1052)												
	0 = 120	VA = 89.94		~H = 7.70								AVG. = 28.2	

INTERPOL LABORATORIES EPA MODIFIED METHOD 5 SAMPLE LOG SHEET

Job L.P. / Hayward, WI
 Source Line 1 / Kovac / Stack
 Cyclone: ☐ Yes ☒ No Filter holder: MMS
 Analytes: PM
 Field recovery spike added: ☒ Yes ☐ No

Date 6-9-94 Test 8 Run 2
 No. of traverse points 24
 Filter type: 4" Glass fiber
 XAD-2 resin: g Batch No.
 Reference: EPA SW-846 Method 0010

Sample Train Leak Check:

Pretest: < 0.02 cfm at 15 in. Hg. (vac) ☒
 Posttest: < 0.02 cfm at 10 in. Hg. (vac) ☒

Semivolatile Catch Data:

No.s of filters used: 348 Recovery solvent(s):
☒ MeCl₂ * ~~Meth (30/70 97v)~~
☒ other(s) Acetone
 No. of bottles for condensate trap catch: 1
 Samples recovered by: Michael

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Condensate trap	<u>404</u>	<u>265</u>	<u>139</u>
Condensate trap			
Condensate trap			
Impingers			
Desiccant	<u>1458</u>	<u>1428</u>	<u>30</u>
Total			<u>169</u>

Integrated Gas Sampling Data:

Bag Pump No. 294 Box No. 27 Bag No. 2
 Bag Material: 4-layer Aluminized Tedlar Size: 44 L
 Pretest leak check: 0 cc/min at 20 in. Hg.
 Time start: 1240 (HRS) Time end: 1534 (HRS)
 Sampling rate: 200 cc/min O₂ Analyzer S/N: 9

INTERPOL LABORATORIES EPA METHOD 16 FIELD DATA SHEET

Job L.P. Hayward Operator MK No. 7 Pitot No. 456
 Source Line 1 House / Stack Meter Box No. 2 Pitot Dia. 1/2 in. 294
 Date 6/2/84 Run 1081 Gas meter const. 996.1 Bar. Pres. 28.90 in. Hg 8 %

Traverse Point No.	Sampling Time (min)	Sample Volume (cc)	Velocity Head (in Hg)	Orifice Meter (in Hg)	Des. Vol. (cc)	VAC. in Hg	Temperature (°F)					Oxygen (%/v)	
							Stack	Probe	Oven	XRD2	Imp.		Meter (in/out)
A-12													
	(1240)	767.51		2.10	1.70	7	318	240	257	42	42	77	15.2
5	5	771.77	.105	2.39	6.16	8	319	244	255	42	41	78	15.1
11	10	776.22	.120	2.31	0.56	8	321	245	260	42	41	79	16.5
10	15	780.62	.116	2.14	4.00	7	320	249	261	42	41	80	16.1
9	20	784.93	.107	2.00	8.92	7	323	252	256	43	42	81	15.2
8	25	788.97	.100	1.81	1.83	6	323	253	259	43	42	82	16.0
7	30	792.94	.090	1.41	6.29	5	324	250	257	44	42	83	14.9
6	35	796.37	.070	1.41	9.76	5	325	247	260	44	42	84	15.1
5	40	799.77	.067	1.35	3.16	5	327	245	261	44	42	84	15.5
4	45	803.15	.060	1.21	6.37	5	329	245	258	45	42	85	13.9
3	50	806.45	.056	1.17	9.54	4.5	329	249	255	45	43	85	13.2
2	55	809.52	.056	1.27	2.93	5	327	248	257	45	43	86	14.1
1	60	812.05	.063	1.02	6.78	2.5	328	245	260	46	43	86	14.2
B-12													
	65	816.75	.090	1.90	0.92	8	329	242	261	47	43	88	15.6
	70	820.92	.094	2.07	5.02	8	331	246	258	46	44	89	14.8
	75	825.00	.103	1.98	9.15	8	331	251	255	46	44	89	13.8
9	80	829.10	.098	1.81	3.09	8	329	248	257	46	44	90	14.0
8	85	833.10	.099	1.70	6.91	7	331	249	260	47	45	90	14.4
7	90	836.97	.084	1.81	0.86	8	329	245	263	47	45	90	14.7
6	95	840.84	.089	1.73	4.72	2.5	329	251	261	47	46	90	15.8
5	100	844.82	.085	1.48	8.30	6	329	253	261	48	46	91	16.2
4	105	848.40	.073	1.42	1.80	6	332	255	259	48	46	91	16.2
3	110	851.84	.070	1.65	5.57	7	330	254	262	44	43	85	16.0
2	115	855.61	.081	1.20	8.76	5.5	331	251	260	44	42	88	16.2
1	120	858.83	.060										
(1534)													
Σ = 120 V _{av} = 91.32 H = 1.71 Avg. = 84.8													

INTERPOL LABORATORIES EPA MODIFIED METHOD 5 SAMPLE LOG SHEET

Job L.P. / Hayward, WI
 Source Line 1 Konus / Stach
 cyclone: ☐ Yes ☒ No Filter holder: MMS
 Analytes: POM
 Field recovery spike added: ☒ Yes ☐ No

Date 6-9-94 Test 8 Run 3
 No. of traverse points 24
 Filter type: 4" Glass fiber
 XAD-2 resin: g Batch No.
 Reference: EPA SW-846 Method 0010

Sample Train Leak Check:

Pretest: 0.02 cfm at 15 in. Hg. (vac) ☐
 Posttest: 2 0.02 cfm at 10 in. Hg. (vac) ☒

Semivolatile Catch Data:

No.s of filters used: 349 Recovery solvent(s)
☒ MeCl₂ * ~~MeOH (50:50 v/v)~~
☒ other(s) Acetone

No. of bottles for condensate trap catch: 1
 Samples recovered by: Mr. Kaehler & K. Rusanthal

Condensate Data:

Item	Weight(g)		
	Final	Tare	Difference
Condensate trap			
Condensate trap	<u>427</u>	<u>267</u>	<u>160</u>
Condensate trap			
Impingers			
Desiccant	<u>1499</u>	<u>1455</u>	<u>44</u>
Total			<u>204</u>

Integrated Gas Sampling Data:

Bag Pump No. 297 Box No. 27 Bag No. 3
 Bag Material: 4-layer Aluminized Tedlar Size: 44 L
 Pretest leak check: 0 cc/min at 20 in. Hg.
 Time start: 1610 (HRS) Time end: 1812 (HRS)
 Sampling rate: 200 cc/min O₂ Analyzer S/N: 9

INTERPOL LABORATORIES EPA W/ FIELD METHOD 3 FIELD WITH SPECT

Job	L.P. / Hayward, w/	Operator	Mr. Kaehle & L. Rosenthal	No 1116 No.	W 815-7	P1101 No.	... 85-6
Source	Line / Strub	Water Box No.	9	No 1116 Dia.	422	Cp	80.04
Date	6-9-94	Test by	Run 3	Bar. Pres.	85.90	H ₂ O	8.3

[illegible]

INTERPOLL LABORATORIES

Benzene Field Data Sheet

Job LPI HAYWARD Operator(s) E. TRIMBRIDGE
 Source LINCOLN KANUS STACK Meter Box No. 25 Meter coef. 1.0078
 Date 6-9-64 Test 9 Run 1 Barometric Pressure 28.90 in.Hg

Sample Train Leak Check:

Pretest: 0 cc/min at 20 in.HgPosttest: 0 cc/min at 20 in.HgBenzene

Trav. Point No.	Samp. Time (min)	Sample Volume (cf)	Sample Rate (cc/min)	VAC. (inHg)	Temperature (oF)		
					Stack	Probe	Gasmeter
	0845	436.910					
	5	437.100	1000	4		—	72
	10	437.280	1000	4			78
	15	437.445	1000	4			84
	20	437.640	1000	4			80
	25	437.899	1000	4			92
	30	438.062	1000	4			96
	35	438.215	1000	4			100
	40	438.368	1000	4			103
	45	438.520	1000	4			105
	50	438.670	1000	4			107
	55	438.860	1000	4			108
	60	439.050	1000	4			109
	$\theta = 60$	$V_m = 2.140$					$t_m = 95.3$

(0845)

$$\sqrt{STO} = 1.981$$

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INTERPOLL LABORATORIES

BENZENE Field Data Sheet

Job LP/Hydrogen Operator(s) ET
 Source LINE 1, Raw Stack Meter Box No. 25 Meter coef. 1.0078
 Date 6-9-94 Test Q Run 2 Barometric Pressure 28.90 in.Hg

Sample Train Leak Check:

Pretest: 0 cc/min at 20 in.HgPosttest: 0 cc/min at 20 in.Hg

Trav. Point No.	Samp. Time (min)	Sample Volume (cf)	Sample Rate (cc/min)	VAC. (inHg)	Temperature (oF)		
					Stack	Probe	Gasmeter
	1000	439.092					
	5	439.245	1000	4			110
	10	439.490	1000	4			115
	15	439.720	1000	4			118
	20	439.890	1000	4			118
	25	440.085	1000	4			118
	30	440.280	1000	4			119
	35	440.470	1000	4			119
	40	440.665	1000	2			120
	45	440.852	1000	4			121
	50	441.042	1000	4			122
	55	441.228	1000	4			124
	60	441.414	1000	4			124
	$\theta = 60$	$V_m = 2.322$					$t_m = 119.0$

(1100)

$$V_{STD} = 2.061$$

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INTERPOL LABORATORIES

BENZENE Field Data Sheet

Job UP/HANDMAID Operator(s) ET
 Source LINE 1 KANUS STACK Meter Box No. 26 Meter coef 1.0078
 Date 6-9-94 Test 2 Run 3 Barometric Pressure 28.90 in.Hg

Sample Train Leak Check:

Pretest: 0 cc/min at 20 in.HgPosttest: 0 cc/min at 20 in.Hg

Trav. Point No.	Samp. Time (min)	Sample Volume (cf)	Sample Rate (cc/min)	VAC. (inHg)	Temperature (oF)		
					Stack	Probe	Gasmeter
	1111	441.480					
	5	441.700	1000	4			124
	10	441.897	1000	4			125
	15	442.085	1000	4			124
	20	442.275	1000	4			105
	25	442.468	1000	4			105
	30	442.645	1000	4			105
	35	442.820	1000	4			105
	40	443.005	1000	4			105
	45	443.170	1000	4			105
	50	443.344	1000	4			105
	55	443.518	1000	4			106
	60	443.688	1000	4			106
	$\theta = 60$	$V_m = 2.208$					$t_m = 1100$

(1320)

 $V_{STD} = 1.991$

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Drawing of Test Site

The diagram shows two views of a cylinder. The top view is a circle with a center point labeled 'O'. It has a small rectangular notch at the top and a small rectangular protrusion at the bottom. The front view is a rectangle with a center point labeled 'C'. It has a small rectangular notch at the top and a small rectangular protrusion at the bottom. The views are labeled 'Cross-section View' and 'Elevation View'.

[illegible]

032594G:STACK\WP\FORMS\S-392.1

INTERPOLL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job L.P. / Hayward, CA Date 6-8-94 Test 16 Run 1
Source Line 2 House / Street No. of traverse points 24
Method 5 Filter holder: Glass Filter type: 4" Pallflex
Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
Post test: 0.02 cfm at 14 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

4035

Recovery solvent(s)

☒ Acetone _____
☐ Other(s) _____

No. of probe wash bottles:

Sample recovered by:

1
Mikaehler & K. Rosenthal

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1	452	394	X58
Impinger No. 2			
Impinger No. 3			
Condenser			
Desiccant	1402	1387	15
Total			X73

Integrated Gas Sampling Data:

Bag Pump No. 29A
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check: 0
Time start: 0757
Sampling rate: 400

Box No. 27 Bag No. 1
Size: 44 L
cc/min at 20 in. Hg.
(HRS) Time end: 0958 (HRS)
cc/min Operator: M. Mikaehler

S/N of O₂ Analyzer used to monitor train outlet:

9

123093-GASTACKIWP\METHODS\S-0046RR

INTERPOL LABIDENTURES

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INTERPOLL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job L.P. / Hayward, Ill
Source Line 2 Rogers / Street
Method 5 Filter holder: 6 hrs
Sample Train Leak Check:

Date 6-8-84 Test 16 Run 2
No. of traverse points 24
Filter type: 4" Pollflex

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
Post test: 0.02 cfm at 19 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

4036

Recovery solvent(s)

☒ Acetone _____
☐ Other(s) _____

No. of probe wash bottles:

Sample recovered by:

1
M. Kachler + K. Rosenthal

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1	<u>460</u>	<u>398</u>	<u>62</u>
Impinger No. 2			
Impinger No. 3			
Condenser			
Desiccant	<u>1480</u>	<u>1464</u>	<u>16</u>
Total			<u>78</u>

Integrated Gas Sampling Data:

Bag Pump No. 29A
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check: 0
Time start: 0920
Sampling rate: 400

Box No. 27 Bag No. 2
Size: 44 L
cc/min at 20 in. Hg.
(HRS) Time end: 1021 (HRS)
cc/min Operator: M. Kachler

S/N of O₂ Analyzer used to monitor train outlet:

9

123093-GASTACK\WP\METHODS\S-0046RR

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INTERPOL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job L.P. / Hayward, WI
Source Line 2 Kerosene / Stuck
Method 5 Filter holder: Glass
Sample Train Leak Check:

Date 6-8-94 Test 16 Run 3
No. of traverse points 24
Filter type: 4" Pallflex

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
Post test: 0.02 cfm at 14 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

4037

Recovery solvent(s)

☒ Acetone _____
☐ other(s) _____

No. of probe wash bottles:

Sample recovered by:

1
M. Koehler + K. Krentzel

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1	462	395	67
Impinger No. 2			
Impinger No. 3			
Condenser			
Desiccant	1420	1402	18
Total			85

Integrated Gas Sampling Data:

Bag Pump No. 29A
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check: 0
Time start: 1114
Sampling rate: 400

Box No. 27 Bag No. 3
Size: 44 L
cc/min at 20 in. Hg.
(HRS) Time end: 1215 (HRS)
cc/min Operator: M. Koehler

S/N of O₂ Analyzer used to monitor train outlet: 9

123093-G:STACK\WPMETHODS\IS-0046RR

Visible Emissions Form

T16

SOURCE NAME <i>Louisiana Pacific</i>				OBSERVATION DATE <i>6-8-94</i>				START TIME <i>9:20</i>				STOP TIME <i>10:21</i>			
ADDRESS <i>RFD 8</i>				SEC MIN				SEC MIN				SEC MIN			
				0 15 30 45				0 15 30 45				0 15 30 45			
CITY <i>Hayward</i>				STATE <i>WI</i>				ZIP <i>54843</i>							
PHONE				SOURCE ID NUMBER											
PROCESS EQUIPMENT <i>Line 2 Korus stack</i>				OPERATING MODE <i>100%</i>											
CONTROL EQUIPMENT <i>ETB</i>				OPERATING MODE <i>100%</i>											
DESCRIBE EMISSION POINT <i>Tallest silver stack at South side of building</i>															
HEIGHT ABOVE GROUND LEVEL <i>START ~100' STOP SAME</i>				HEIGHT RELATIVE TO OBSERVER <i>START ~100' STOP SAME</i>											
DISTANCE FROM OBSERVER <i>START ~300' STOP SAME</i>				DIRECTION FROM OBSERVER <i>START ~360° STOP SAME</i>											
DESCRIBE EMISSIONS <i>START Coning Plume STOP SAME</i>															
EMISSION COLOR <i>START White STOP SAME</i>				PLUME TYPE: CONTINUOUS ☒ FUGITIVE ☐ INTERMITTENT ☐											
WATER DROPLETS PRESENT: <i>NO YES</i>				IF WATER DROPLET PLUME: ATTACHED ☐ DETACHED ☐											
POINT IN THE PLUME AT WHICH OPACITY WAS DETERMINED <i>START Directly above stack Exit STOP SAME</i>															
DESCRIBE BACKGROUND <i>START Clear Blue Sky STOP SAME</i>															
BACKGROUND COLOR <i>START Blue STOP SAME</i>				SKY CONDITIONS <i>START Clear STOP SAME</i>											
WIND SPEED <i>START 15 mph STOP SAME</i>				WIND DIRECTION <i>START E-NE STOP SAME</i>											
AMBIENT TEMP <i>START 72°F STOP SAME</i>				WET BULB TEMP. <i>63°F</i>				RH, percent <i>72%</i>							
				24				54				5			
				25				55				5			
				26				56				5			
				27				57				5			
				28				58				5			
				29				59				5			
				30				60				5			
				AVERAGE OPACITY FOR HIGHEST PERIOD				NUMBER OF READINGS ABOVE % WERE							
				RANGE OF OPACITY READINGS MINIMUM 0				MAXIMUM 5							
				OBSERVER'S NAME (PRINT) <i>Edward J. Jurs III</i>											
OBSERVER'S SIGNATURE <i>[Signature]</i>				DATE <i>6-8-94</i>											
ORGANIZATION <i>Interpoll Labs, Inc.</i>															
I HAVE RECEIVED A COPY OF THESE OPACITY OBSERVATIONS SIGNATURE				CERTIFIED BY <i>Eastern Tech. Assoc.</i>				DATE <i>6-8-94</i>							
TITLE				DATE				VERIFIED BY							

Interpoll Laboratories
(612)786-6020

EPA Method 7 Sample Collection
Field Data Sheet

Job LP / HAYWARD Date 6-8-94 Bar. Pressure 28.98 IN.HG.
Test Location LINE 2 Fuel Type WOOD Sample Train No. GREEN
Technician KR Pump No. 298

No.	Test Run Point	Flask No.	Time (HRS)	Vacuum (IN.HG.)	Flask Temp. (°F)	Leak Rate <0.4 IN.HG./MIN.
1	16-1-3	13	0800	27.4	59	☒ Yes ☐ No
2	16-1-2	14	0815	27.3	59	☒ Yes ☐ No
3	16-1-1	15	0830	27.4	59	☒ Yes ☐ No
4	16-1-1	16	0845	27.4	60	☒ Yes ☐ No
5	16-2-2	17	0920	27.3	60	☒ Yes ☐ No
6	16-2-3	18	0935	27.3	60	☒ Yes ☐ No
7	16-2-3	55	0950	27.3	60	☒ Yes ☐ No
8	16-2-2	56	1005	27.3	60	☒ Yes ☐ No
9	16-3-1	57	1115	27.3	64	☒ Yes ☐ No
10	16-3-1	58	1130	27.2	65	☒ Yes ☐ No
11	16-3-2	59	1145	27.3	65	☒ Yes ☐ No
12	16-3-3	60	1200	27.3	65	☒ Yes ☐ No
13						☐ Yes ☐ No
14						☐ Yes ☐ No
15						☐ Yes ☐ No
16						☐ Yes ☐ No
17						☐ Yes ☐ No
18						☐ Yes ☐ No
19						☐ Yes ☐ No
20						☐ Yes ☐ No
21						☐ Yes ☐ No
22						☐ Yes ☐ No
23						☐ Yes ☐ No
24						☐ Yes ☐ No
25						☐ Yes ☐ No
26						☐ Yes ☐ No
27						☐ Yes ☐ No

Drawing of Test Site

R or nothing = reg. manometer; S = expanded; E = electronic

INTERPOLL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job L.P. / Hayward, WI Date 6-8-94 Test 17 Run 1
Source Line 2 Kenosha / Stach No. of traverse points 24
Method poll Filter holder: NA Filter type: NA
Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
Post test: 0.02 cfm at 10 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

NA

Recovery solvent(s)

☐ acetone
☒ other(s) MeCl₂

No. of probe wash bottles:

0

Sample recovered by:

M. Kachler + K. Rosenthal

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1	<u>531</u>	<u>477</u>	<u>54</u>
Impinger No. 2			
Impinger No. 3			
Condenser			
Desiccant	<u>1497</u>	<u>1480</u>	<u>17</u>
Total			<u>71</u>

Integrated Gas Sampling Data:

Bag Pump No. 294
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check: 0
Time start: 1446
Sampling rate: 400

Box No. 25 Bag No. 1
Size: 44 L
cc/min at 20 in. Hg.
(HRS) Time end: 1553 (HRS)
cc/min Operator: M. Kachler

S/N of O₂ Analyzer used to monitor train outlet:

9

INTERPOL LABORATORIES EPA METHOD 5 FIELD DATA SHEET

Job L.P. / Hayward, CA Operator Michael J. K. Ruggenthal Pilot No. 290-5 Ep 04
 Sample Line 100 ft Meter Box No. 9 Bar. Pressure 28.98 InHg 1120 2.8 X
 Date 6-8-94 Cassette Count 17 Hum 1 Cassette No. 6455-6 Hertz 10 168

Traverse Point No.	Sampling Time (min)	Sample Volume (cf)	Velocity Head (inHg)	Orifices Meter (inHg)	Dep. Vol. (cf)	VAC. InHg	Temperature (°F)				Gas/Dol	Dry/Wet (X/V/V)
							Stack	Probe	Dry	Wet		
A-12	144.6	503.60	.21	2.42	5.85	5	324	243	248	41	80	17.3
11	2.5	505.07	.21	2.42	8.10	5	325				81	17.1
10	7.5	510.31	.20	2.31	0.29	5	325	147	245	40	81	17.1
9	10	512.54	.19	2.21	2.45	5	322				85	17.0
8	12.5	514.55	.17	1.97	9.49	5	325	248	251	40	86	17.0
7	15	516.52	.16	1.86	6.47	4	325				88	16.7
6	17.5	518.55	.17	1.98	8.52	4.5	325	245	255	40	89	16.8
5	20	520.92	.13	2.67	0.89	6	327				90	16.9
4	22.5	523.33	.13	2.68	3.27	6	327	242	254	42	91	17.0
3	25	525.78	.14	2.79	5.70	6	329				92	17.5
2	27.5	528.10	.14	2.81	8.14	6	325	247	256	42	93	17.4
1	30	530.57	.13	2.69	0.53	6	327				93	16.6
B-12	32.5	532.54	.15	1.75	2.46	4	330	251	257	43	91	16.4
11	35	534.60	.19	2.23	4.63	5	324				94	16.2
10	37.5	536.72	.16	1.88	6.64	4	325	255	255	43	90	16.6
9	40	538.70	.16	1.97	8.63	4	325				92	16.3
8	42.5	540.60	.15	1.76	0.57	4	326	252	258	43	94	16.3
7	45	542.49	.14	1.64	2.44	3.5	327				94	16.4
6	47.5	544.45	.17	1.99	4.51	4	327	253	261	43	95	16.0
5	50	546.55	.17	2.00	6.57	4	326				96	16.7
4	52.5	549.05	.25	2.93	9.07	6.5	329				97	16.5
3	55	551.56	.25	2.93	1.57	6.5	329				98	16.1
2	57.5	554.10	.25	2.94	4.08	6.5	329	247	258	43	98	16.0
1	60	556.58	.14	2.83	6.54	6	327				98	15.6
V = 52.98												
(1553)												
0 = 60												
Avg. = 88.1												

INTERPOLL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job L.P. / Hayward, WI Date 6-8-84 Test 17 Run 2
Source Line 2 Korus / Stack No. of traverse points 24
Method CO11 Filter holder: NA Filter type: NA
Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
Post test: 0.02 cfm at 10 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

NA

Recovery solvent(s)

☐ acetone
☒ Other(s) MeCl₂

No. of probe wash bottles:

Sample recovered by:

0
M. Kaehler & K. Rosenthal

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1	55 533	481	52
Impinger No. 2			
Impinger No. 3			
Condenser			
Desiccant	1508	1491	17
Total			69

Integrated Gas Sampling Data:

Bag Pump No. 29 A
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check: 0
Time start: 1616
Sampling rate: 400

Box No. 25 Bag No. 2
Size: 4.4 L
cc/min at 20 in. Hg.
(HRS) Time end: 1718 (HRS)
cc/min Operator: M. Kaehler

S/N of O₂ Analyzer used to monitor train outlet:

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INTERPOL LABORDRAIDRIES EPA METHOD 5 FIELD DATA SHEET

Job B.P. / Hayward, CA
 Source Line 2 Kanus / Street
 Date 6-8-94

Operator Paul K. Gabel & K. K. Gabel
 Meter Box No. 9901
 Recorder Code 17

Pilot No. 22V-5 Ep. 04
 Bar. Pres. 28.98 Hg. 120
 Nozzle No. Class Nozzle Dia. 3.00 IN.

Traverse Point No.	Sampling Time (min)	Supply Volume (ft ³)	Velocity Head (inches)	Orifice Meter (inches)	Det. Vol. (ft ³)	VAD. (inches)	Temperature (°F)				Dwyer (°F)
							Stack	Probe	Dry	Wet	
B-12	16.16	556.90	.120	2.39	9.15	5.5	329	243	244	43	87
11	5	559.13	.14	1.67	1.03	3.5	329				86
10	2.5	561.07	.16	1.91	3.05	4	328	244	251	43	87
9	10	563.06	.15	1.80	5.01	4	326				87
8	12.5	565.09	.13	1.57	6.84	3	326	247	255	44	88
7	15	566.87	.13	1.57	8.67	3	324				88
6	17.5	570.84	.17	2.06	0.77	4	324	249	254	44	88
5	20	572.95	.18	2.18	2.93	4.5	323				89
4	22.5	575.40	.23	2.80	5.38	6	323	246	258	44	90
3	25	577.82	.23	2.80	2.83	6	323				90
2	27.5	580.18	.23	2.80	0.28	6	323	244	255	44	90
1	30	582.76	.23	2.80	1.73	6	323				90
A-12	32.5	584.99	.19	2.32	4.96	5	322	247	253	46	91
11	35	587.30	.20	2.43	2.24	5	323				91
10	37.5	589.15	.19	2.32	2.48	5	321	251	250	46	91
9	40	591.79	.19	2.32	1.71	5	321				91
8	42.5	593.77	.15	1.83	3.70	4	324	248	253	46	92
7	45	595.80	.16	1.95	5.75	4	324				92
6	47.5	598.10	.14	2.32	2.99	5	324	245	255	46	92
5	50	600.44	.21	2.56	0.33	6	324				92
4	52.5	602.77	.22	2.69	2.74	6	324	249	252	47	93
3	55	605.16	.21	2.57	5.09	6	325				93
2	57.5	607.50	.21	2.57	2.45	6	324	253	252	47	93
1	60	609.83	.20	2.46	9.75	5.5	321				93
		Σ = 52.93		Σ = 2.28							Av. = 93.9
		0 = 60									

INTERPOLL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job L.P. / Hayward, WI Date 6-8-94 Test 17 Run 3
Source Line 2 Kenosha No. of traverse points 24
Method 0011 Filter holder: NA Filter type: NA
Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 in. Hg. (vac) ☒
Post test: 0.02 cfm at 10 in. Hg. (vac) ☒

Particulate Catch Data:

No. of filters used:

NA

Recovery solvent(s)

☐ acetone
☒ Other(s) MeCl₂

No. of probe wash bottles:
Sample recovered by:

0
M. Kachler + R. Rosenthal

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1	542	493	59
Impinger No. 2			
Impinger No. 3			
Condenser			
Desiccant	1514	1497	17
Total			76

Integrated Gas Sampling Data:

Bag Pump No. 29A
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check: 0
Time start: 1742
Sampling rate: 400

Box No. 25 Bag No. 3
Size: 44 L
cc/min at 20 in. Hg.
(HRS) Time end: 1943 (HRS)
cc/min Operator: M. Kachler

S/N of O₂ Analyzer used to monitor train outlet:

9

123093-GASTACK\WP\METHODS\0046RR

INTERPOL LABORATORIES EPA METHOD 5 FIELD DATA SHEET

Lab L.P. / Hayward, Cal
 Source Single Manure / Stack
 Date 6-8-94 Run 3

Operator Mark Kachigian
 Motor Box No. 118
 Counter Count 9961

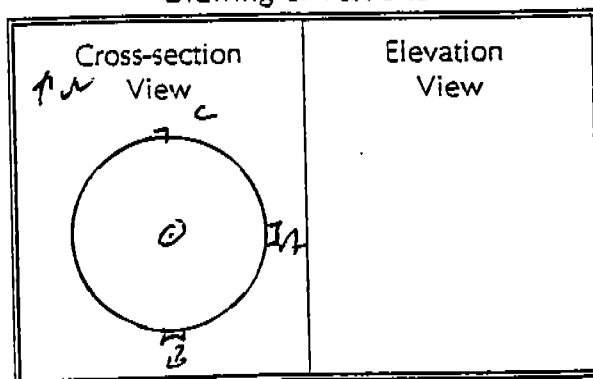
Pilot No. 220-5 Ep 103
 Bar. Press. 28.98 InHg 1120
 Humidity No. 6456 Relative D.H. 308

Transfer Point No.	Sampling Time (min)	Sample Volume (cc)	Velocity Hood (in/min)	Orifice Meter (in/min)	Obs. Vol. (cc)	VAC. inHg	Temperature (°F)						Corr'n	Corr'Dep	Observed (cc)	Dry Bulb (°F)
							Stack	Probe	Down	Leaky	Gas In	Gas/Dup				
B-12	1742	610.10														
	2.5	612.35	.10	2.44	2.38	5	323	243	257	43	88	88			16.2	
	5	614.62	.10	2.42	4.65	5	322				91	88			16.3	
	7.5	616.79	.17	2.07	6.74	4	320	240	255	42	93	89			16.2	
	10	618.67	.13	1.58	8.58	3	321				94	89			16.4	
9	12.5	620.73	.16	1.95	0.63	4	320	245	258	43	95	89			16.3	
7	15	622.93	.19	2.32	2.85	5	320				96	89			16.6	
6	17.5	625.40	.23	2.80	5.30	6	321	251	260	44	97	89			17.0	
5	10	627.84	.23	2.80	7.75	6	322				98	90			17.1	
4	22.5	630.50	.30	3.66	0.54	8	321	248	262	44	97	90			15.8	
3	15	633.31	.30	3.66	3.33	8	321				97	89			16.2	
2	27.5	636.07	.29	3.54	6.08	8	320	245	257	45	98	90			16.4	
1	30	638.82	.27	3.29	8.73	7.5	321				98	90			16.4	
A-12	34.5	641.22	.23	2.81	1.19	6	310	250	257	45	96	89			16.9	
	35	643.77	.24	2.93	3.69	6	320				97	90			16.7	
	37.5	646.05	.20	2.44	5.98	5	321	247	255	46	98	90			16.5	
	40	648.20	.18	2.20	8.15	5	322				99	90			17.1	
	42.5	650.30	.17	2.07	0.26	4	325	244	258	46	99	90			17.2	
7	45	652.45	.18	2.21	2.43	5	320				99	91			17.0	
6	42.5	655.10	.25	3.07	5.00	6.5	319	243	259	46	100	91			17.0	
5	50	657.65	.27	3.31	2.66	7	320				101	91			17.2	
4	52.5	660.40	.29	3.55	0.42	7.5	321	247	255	46	101	91			17.0	
3	55	663.30	.31	3.80	3.28	8.5	319				100	91			16.8	
2	57.5	665.04	.28	3.44	5.99	7.5	319	245	252	46	99	91			16.7	
1	60	668.44	.22	2.70	8.40	6	318				99	91			17.1	
		V = 58.34		2.79											Avg. = 93.4	
		0 = 60														
		(1843)														

INTERPOLL LABORATORIES, INC.
(612) 786-6020
EPA Method 2 Field Data Sheet

Drawing of Test Site

Job H.P. / Hayward, WI
Source Line 2 Kanus / Stack
Test 18 Run 0 Date 6-8-94
Stack Dimen. 51.5 IN.
Dry Bulb 32.5 °F Wet bulb 13.0 °F
Manometer ☒ Reg. ☐ Exp ☐ Elec.
Barometric Pressure 28.98 IN.HG
Static Pressure -.28 IN.WC
Operators M. Kumbler & 16 Assistant
Pitot No. 29-6 C. BA VA

[illegible]

R or nothing = reg. manometer; S = expanded; E = electronic

032594-G:STACK/WP/FORMS-392.1

INTERPOL LABORATORIES
EPA Method 4 and 6 Field Data Sheet

Job 2. P. / Hayward, Cal
Source Line 2 House / Stack
Date 6-8-94 Test 18 Run 1

Operator(s) M. Kaehler + K. Rosenthal
Meter Box No. 10 Gasmeter coef. 19930
 ΔH 1.77 in.WC Bar. press 28.95 in.Hg

Sample Train Leak Check:

Pretest: < 0.02 cfm at 15 in. Hg. 8
Posttest: 60.02 cfm at 10 in. Hg. 8

Trav. Point No.	Samp. Time (min)	Sample Volume (cf)	Orif. Meter (inWC)	VAC. inHg	Temperatures (°F)					Oxygen (%v/v)
					Probe	Oven	Impg.	Gas/In	Gas/Out	
	1447	578.60								
C-3	5	582.47	1.77	7	247	250	40	74	73	17.6
3	10	586.30	1.77	7	243	254	40	79	73	17.0
3	15	590.12	1.77	7	243	251	40	83	74	16.7
3	20	593.94	1.77	7	245	256	40	86	74	16.6
2	25	597.73	1.77	7	241	258	41	88	75	17.1
2	30	601.53	1.77	7	246	261	41	90	76	17.4
2	35	605.33	1.77	7	253	257	41	90	76	16.3
2	40	609.13	1.77	7	250	256	41	86	77	16.3
1	45	612.96	1.77	7	244	260	43	89	77	16.1
1	50	616.78	1.77	7	242	263	45	91	78	16.1
1	55	620.50	1.77	7	248	261	45	92	78	16.4
1	60	624.30	1.77	7	249	259	45	93	79	15.5
(1554)										
	$\theta = 60$	$V_m = 45.70$	$(\Delta H)_{avg} = 1.77$					$(t_m)_{avg} = 81.29$		

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger A	313	268	45
Condenser Impinger B	275	268	7
Desiccant	1450	1432	18
Total			70

Preliminary results of SO ₂ concentration determination	
V _{std}	= 43.07 DSCF
Moisture	= 7.11 %v/v
SO ₂ , dry	= ppm
SO ₂ , wet	= ppm
LB/MMBtu	=

INTERPOL LABORATORIES
EPA Method 4 and 6 Field Data Sheet

Job L.P. / Hayward, WI
Source Line 2 / Keweenaw / Stack
Date 6-8-94 Test 19 Run 2

Operator(s) Michael & K. Rucinski
Meter Box No. 10 Gas meter coef. 9930
Orifice 1.77 in. WC Bar. press 16.78 in. Hg

Sample Train Leak Check:

Pretest: < 0.02 cfm at 15 in. Hg.
Posttest: < 0.02 cfm at 10 in. Hg.

Trav. Point No.	Samp. Time (min)	Sample Volume (cf)	Orif. Meter (inWC)	VAC. inHg	Temperatures (°F)					Oxygen
					Probe	Oven	Impg.	Gas/In	Gas/Out	(%v/v)
	1617	624.70								
C-3	5	628.53	1.77	7	247	253	43	81	80	16.7
3	10	632.36	1.77	7	252	260	43	86	79	16.5
3	15	636.22	1.77	7	248	263	44	89	79	16.7
3	20	640.08	1.77	7	245	257	44	91	79	17.0
2	25	643.97	1.77	7	241	253	46	93	80	16.6
2	30	647.71	1.77	7	246	255	46	94	80	16.4
2	35	651.55	1.77	7	250	257	46	92	81	16.6
2	40	655.42	1.77	7	249	260	46	95	81	16.8
1	45	659.30	1.77	7	246	263	46	95	82	16.6
1	50	663.09	1.77	7	249	260	46	96	82	16.7
1	55	666.84	1.77	7	253	258	47	96	82	16.5
1	60	670.66	1.77	7	250	255	47	96	83	16.3
	(1718)									
	θ = 60	V _m = 45.96	([^] H) = 7.77					(t _m) _{avg} = 86.33		

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger A	310	267	43
Condenser Impinger B	277	269	8
Desiccant	1434	1420	14
		Total	65

Preliminary results of SO ₂ concentration determination	
V _{std}	= 42.91 DSCF
Moisture	= 6.66 %v/v
SO ₂ , dry	= ppm
SO ₂ , wet	= ppm
LB/MMBtu	=

INTERPOL LABORATORIES
EPA Method 4 and 6 Field Data Sheet

Job L.P. / Hayward, CA
Source Line 2 Hous / Stack
Date 6-8-94 Test 18 Run 3

Operator(s) Michael K. Rosenthal
Meter Box No. 10 Gas meter coef. 9930
 $\bar{P}_{HG}$ 1.77 in.WC Bar. press 28.98 in.Hg

Sample Train Leak Check:

Pretest: < 0.02 cfm at 15 in. Hg.
Posttest: < 0.02 cfm at 10 in. Hg.

Trav. Point No.	Samp. Time (min)	Sample Volume (cf)	Orif. Meter (inWC)	VAC. inHg	Temperatures (°F)					Oxygen
					Probe	Oven	Impg.	Gas/In	Gas/Out	(%v/v)
	1743	671.30								
C-3	5	675.20	1.77	7	245	255	45	93	92	16.2
3	10	679.08	1.77	7	250	252	45	97	92	16.3
3	15	692.99	1.77	7	253	250	45	90	92	16.3
3	20	686.87	1.77	7	255	247	45	92	92	17.3
2	25	690.74	1.77	7	251	253	46	93	92	16.3
2	30	694.60	1.77	7	248	256	46	94	92	16.8
2	35	698.49	1.77	7	245	255	46	92	92	16.9
2	40	702.33	1.77	7	243	258	46	95	92	16.8
1	45	706.17	1.77	7	248	260	48	95	93	17.2
1	50	710.00	1.77	7	245	263	48	96	93	17.3
1	55	713.85	1.77	7	247	263	48	96	93	17.2
1	60	717.65	1.77	7	250	259	48	96	93	17.1
(1844)										
	$\theta = 60$	$V_m = 46.35$	$(\bar{P}_{HG})_{ave} = 1.77$					$(t_m)_{ave} = 87.38$		

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impingers A	307	267	40
Condenser Impinger B	274	266	8
Desiccant	1465	1450	15
Total			63

Preliminary results of SO₂ concentration determination

$V_{std} = 43.19$ DSCF

Moisture = 6.43 %v/v

SO₂, dry = ppm

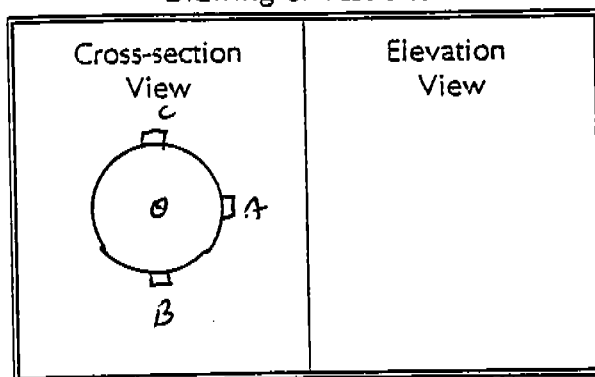
SO₂, wet = ppm

LB/MMBtu =

INTERPOLL LABORATORIES, INC.
(612) 786-6020
EPA Method 2 Field Data Sheet

Drawing of Test Site

Job L.P. / Hayward, Ill.
Source Line 2 Home / Street
Test 19 Run 0 Date 6-7-94
Stack Dimen. 51.5 IN.
Dry Bulb 329 °F Wet bulb 130 °F
Manometer ☐ Reg. ☐ Exp ☐ Elec.
Barometric Pressure 28.73 IN.HG
Static Pressure - .26 IN.WC
Operators M. Kachler + K. Rosenthal
Pitor No. MM5-6 C_p .94



POM

Traverse Point No.	Fraction of Diameter	Distance From Stack Wall (IN.)	Distance From End of Port (IN.)	Velocity	Temp. of Gas (°F)
		Port Length: <u>3.5</u> IN.	Time Start: <u>0800</u> HRS		
A-1	.021	1.08	4.58	.30	
2	.067	3.45	6.95	.32	
3	.119	6.08	9.58	.33	
4	.177	9.12	12.62	.31	
5	.250	12.88	16.38	.29	
6	.356	19.33	21.83	.25	
7	.644	33.17	36.67	.20	329
8	.750	39.63	42.13	.20	
9	.913	42.38	45.99	.20	
10	.892	45.42	48.92	.21	
11	.933	48.05	51.55	.23	
12	.979	50.42	53.92	.23	
B-1				.26	
2				.25	
3				.28	
4				.29	
5				.31	327
6				.32	
7		35.49 ft/sec		.28	
8		46 FM 30.911		.26	
9		DSL-F-M 19005		.20	
10				.24	
11				.24	
12				.22	
Temp. Meas. Device & S/N: <u>PDT-31 / TR</u>				Time End: <u>0809</u> HRS	

R or nothing = reg. manometer; S = expanded; E = electronic

INTERPOL LABORATORIES EPA MODIFIED METHOD 5 SAMPLE LOG SHEET

Job L.P. / Hayward, WI
 Source Line 2 Konus / Stack
 Cyclone: ☐ Yes ☒ No Filter holder: MMS
 Analytes: POM
 Field recovery spike added: ☒ Yes ☐ No

Date 6-7-94 Test 19 Run 1
 No. of traverse points 24
 Filter type: 4" Glass fiber
 XAD-2 resin: g Batch No.
 Reference: EPA SW-846 Method 8010

Sample Train Leak Check:

Pretest: 0.02 cfm at 15 in. Hg. (vac) ☒
 Posttest: 0.02 cfm at 15 in. Hg. (vac) ☒

Semivolatile Catch Data:

No.s of filters used: 0343 Recovery solvent(s):

☒ MeCl₂ * MeOH (~~50:50 v/v~~)
☒ other(s) Acetone

No. of bottles for condensate trap catch: 1
 Samples recovered by: Mikachler + K. Rosenthal

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Condensate trap	436	264	172
Condensate trap			
Condensate trap			
Impingers	1438	1414	24
Desiccant	1408	1399	9
Total			205

Integrated Gas Sampling Data:

Bag Pump No. 294 Box No. 1 Bag No. 1
 Bag Material: 4-layer Aluminized Tedlar Size: 44 L
 Pretest leak check: 0 cc/min at 20 in. Hg.
 Time start: 0927 (HRS) Time end: 1032 (HRS)
 Sampling rate: 200 cc/min O₂ Analyzer S/N: 9

JOB L.P. / Hagaland, Ill
 SOURCE Line 2 Radio Stack
 DATE 6-7-64 pg 1 AUG 1

Operator M. Kuehler t. A. Rosenthal
 Meter Box No. 9
 Gas meter count. 19961

NOT16 No. AMS-6
 NOT16 Dia. 36.4 in.
 Bar. Pres. 28.73 in. Hg

P101 No. 5-6
 CP EV
 H₂O 9 %

[illegible]

INTERPOLL LABORATORIES EPA MODIFIED METHOD 5 SAMPLE LOG SHEET

Job L.P. / Hayward, WI
 Source Line 2 Kenosha / Stach
 Cyclone: ☐ Yes ☒ No Filter holder: MMS
 Analytes: POH
 Field recovery spike added: ☒ Yes ☐ No

Date 6-7-94 Test 19 Run 2
 No. of traverse points 24
 Filter type: 4" Glass fiber
 XAD-2 resin: g Batch No.
 Reference: EPA SW-846 Method 0010

Sample Train Leak Check:

Pretest: < 0.02 cfm at 15 in. Hg. (vac) go
 Posttest: 20.02 cfm at 19 in. Hg. (vac) go

Semivolatile Catch Data:

No.s of filters used: 0344 Recovery solvent(s)

☒ MeCl₂ * ~~MeOH~~ (50:50 v/v)
☒ other(s) Acetone

No. of bottles for condensate trap catch: 1
 Samples recovered by: M. Kuscha + R. Reventhal

Condensate Data:

Item	Weight(g)		
	Final	Tare	Difference
Condensate trap			
Condensate trap	<u>422</u>	<u>264</u>	<u>158</u>
Condensate trap			
Impingers			
Desiccant	<u>1497</u>	<u>1450</u>	<u>37</u>
Total			<u>195</u>

Integrated Gas Sampling Data:

Bag Pump No. 294 Box No. 1 Bag No. 2
 Bag Material: 4-layer Aluminized Tedlar Size: 44 L
 Pretest leak check: 0 cc/min at 20 in. Hg.
 Time start: 1136 (HRS) Time end: 1342 (HRS)
 Sampling rate: 200 cc/min O₂ Analyzer S/N: 9

INTERPOL LABORATORIES EPA METHOD 3 FIELD DATA SHEET

Job L.P. / Hayward, CA Operator M. Kaehler No. 2115-6 P1101 No. 2115-6
 Source Line 1 / Kapi / Stack Meter Box No. 9 Nozzle Dia. 3/64 in. Cp. 1.54
 Date 6-7-94 1081 14 / JUN 2 Gasometer coeff. .9961 Bar. Pres. 20.73 in. Hg H₂O 0.3 %

Traverse Point No.	Sampling Time (min)	Sample Volume (cc)	Velocity Head (in H ₂ O)	Orifice Meter (in H ₂ O)	Dep. Vol. (cc)	VAC. in Hg	Temperatures (°F)						Oxygen (% v/v)
							Stack	Probe	Orifice	XAD2	Lap.	Meter (in/out)	
A-12													
	1136	111.00					331	247	255	44	42	75	16.5
A-12	5	115.89	.26	2.79	5.03	12	335	254	264	42	39	76	16.5
11	10	120.68	.27	2.87	0.72	12	337	249	248	43	40	77	16.7
10	15	125.60	.26	2.77	5.54	12	334	245	248	43	40	78	16.1
9	20	130.07	.22	2.36	0.00	10.5	334	246	240	43	40	79	15.7
8	25	134.56	.22	2.37	4.46	10.5	333	246	235	43	41	79	16.1
7	30	138.81	.20	2.16	8.74	10	337	243	234	43	41	80	15.5
6	35	142.97	.19	2.05	2.91	9.5	339	247	234	43	41	80	16.1
5	40	147.63	.24	2.58	2.58	11	339	247	248	44	42	82	16.5
4	45	152.52	.27	2.91	2.55	13	336	242	253	44	42	82	16.8
3	50	157.85	.29	3.24	2.88	15	336	245	249	44	42	82	16.5
2	55	163.00	.30	3.24	3.04	14	337	245	247	44	42	82	16.1
1	60	168.22	.30	3.24	8.29	14.5	335	248	253	45	43	83	15.3
B-12	65	172.86	.23	2.49	2.90	13	341	246	251	45	43	83	15.7
11	70	177.52	.24	2.59	2.98	13	341	242	250	45	43	85	16.7
10	75	182.05	.22	2.37	2.07	11.5	340	240	248	44	43	86	16.8
9	80	186.30	.19	2.05	6.26	10	341	245	251	44	43	87	16.8
8	85	190.42	.18	1.96	0.36	10	342	242	253	44	43	88	16.5
7	90	194.41	.17	1.85	4.35	9.5	342	243	250	44	43	88	16.7
6	95	198.80	.21	2.29	8.79	11	343	247	252	44	43	88	16.8
5	100	203.80	.27	2.94	3.83	15	342	247	256	44	43	88	16.5
4	105	209.15	.30	3.29	9.15	17	343	247	256	44	43	88	16.7
3	110	214.67	.33	3.69	4.71	18	341	241	253	44	43	87	16.8
2	115	220.50	.32	3.48	0.57	17	341	241	253	44	43	87	16.5
1	120	225.57	.32	3.49	5.66	17							
(1342)													
Σ		1141.57		2.71									
0 =													
Avg. =		86.1											

INTERPOL LABORATORIES EPA MODIFIED METHOD 5 SAMPLE LOG SHEET

Job L.P. / Hayward, WI
 Source Line 2 Kenos / Stuck
 Cyclone: ☐ Yes ☒ No Filter holder: MMS
 Analytes: POH
 Field recovery spike added: ☒ Yes ☐ No

Date 6-7-94 Test 19 Run 3
 No. of traverse points 24
 Filter type: 4" Glass fiber
 XAD-2 resin: g Batch No.
 Reference: EPA SW-846 Method 0010

Sample Train Leak Check:

Pretest: < 0.02 cfm at 15 in. Hg. (vac) ☒
 Posttest: 20.02 cfm at 19 in. Hg. (vac) ☒

Semivolatile Catch Data:

No.s of filters used: 0345 Recovery solvent(s)
☒ MeCl₂ * MeOH (50:50 v/v)
☒ other(s) Acetone

No. of bottles for condensate trap catch: 1
 Samples recovered by: M. Kachler + K. Krentholtz

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Condensate trap			
Condensate trap			
Condensate trap			
Impingers	<u>401</u>	<u>264</u>	<u>137</u>
Desiccant	<u>1469</u>	<u>1408</u>	<u>61</u>
Total			<u>198</u>

Integrated Gas Sampling Data:

Bag Pump No. 294 Box No. 1 Bag No. 3
 Bag Material: 4-layer Aluminized Tedlar Size: 44 L
 Pretest leak check: 0 cc/min at 20 in. Hg.
 Time start: 1425 (HRS) Time end: 1627 (HRS)
 Sampling rate: 200 cc/min O₂ Analyzer S/N: 9

INTERPOL LABORATORIES EPA MD: IED METHOD 3 FIELD DATA SHEET

JOB L.P. 1 Hayward, Cal OPERATORS M. Kachler & K. Kowalski NO. 4415-6 P1101 NO. 4415-6
 SOURCE Line 2 Roofs / Stack METER BOX NO. 9 NO. 364 IN. 1A CP 04
 DATE 6-7-84 TIME 14 HRS 3 GAS METER COST. 9961 BAR. PRES. 28.23 IN. HG 7.9 %

Traverse Point No.	Sampling Time (min)	Sample Volume (cc)	Velocity Head (in Hg)	Orifice Meter (in Hg)	Doe. Vol. (cc)	VAC. in Hg	Temperature (°F)					Oxygen (% v/v)	
							Stack	Probe	Oven	XRAD	log.		Meter (In/Out)
B-12	1425	225.90					331	243	251	42	40	82	17.6
11	5	230.47	.23	2.53	0.54	10	333	240	254	42	40	85	16.9
10	10	235.21	.24	2.61	5.24	10.5	337	245	255	42	40	88	17.1
9	15	239.80	.22	2.39	9.74	10	336	241	252	43	40	90	17.2
8	20	244.10	.20	2.18	4.08	9	336	245	242	41	39	91	17.8
7	25	248.30	.19	2.08	8.27	8	340	249	235	41	39	92	17.8
6	30	252.53	.19	2.07	2.48	8	337	244	238	41	39	93	17.6
5	35	257.12	.22	2.41	2.02	9.5	338	247	243	40	39	94	17.8
4	40	261.45	.20	2.19	1.35	9	335	250	244	40	39	94	17.3
3	45	266.55	.26	3.08	6.49	12.5	337	246	248	40	39	94	17.2
2	50	271.87	.30	3.29	1.80	14	338	247	252	40	40	94	17.3
1	55	277.45	.33	3.61	7.36	16	332	243	250	40	40	94	17.0
A-12	65	287.70	.25	2.75	2.63	12	335	245	256	42	40	90	17.3
11	70	292.70	.27	2.96	2.65	13	335	240	257	42	40	94	17.0
10	75	297.68	.26	2.89	2.63	12	328	237	254	42	41	95	17.1
9	80	302.67	.27	3.00	2.70	13	329	241	253	43	41	97	16.9
8	85	307.37	.22	2.45	2.29	11	329	244	250	43	41	97	17.4
7	90	311.73	.20	2.24	1.69	9.5	326	245	254	43	41	97	17.1
6	95	316.55	.25	2.79	6.59	12.5	326	247	253	43	41	98	16.5
5	100	322.00	.31	3.46	2.05	15	327	247	250	43	41	98	16.7
4	105	327.55	.32	3.56	2.58	16	329	251	250	44	42	96	16.5
3	110	332.18	.28	3.12	2.76	15.5	327	250	254	44	42	94	16.1
2	115	337.90	.27	3.01	2.84	14	325	247	253	44	42	94	16.2
1	120	342.80	.27	3.01	2.92	14	326	244	250	44	43	94	16.1
	1627												
Total		VB = 117.00		VB = 80								AVG. = 99.3	
0 = 120													

INTERPOLL LABORATORIES

Benzene Field Data Sheet

Job L.P. / Hayward, WI
 Source Line 2 Korus / Stack
 Date 6-7-94 Test 20 Run 1

Operator(s) M. Kaehler + K. Rosenthal
 Meter Box No. 55 Meter coef. 1.0015
 Barometric Pressure 29.73 in.Hg

Sample Train Leak Check:

Pretest: 0 cc/min at 20 in.Hg

Posttest: 0 cc/min at 16 in.Hg

Trav. Point No.	Samp. Time (min)	Sample Volume (cf)	Sample Rate (cc/min)	VAC. (inHg)	Temperature (=F)		
					Stack	Probe	Gasmeter
	0949	921.500					
C-3	5	921.697	1000	3	334	NA	70
3	10	921.880	1000	3	334		71
3	15	922.063	1000	3	334		73
3	20	922.250	1000	3	334		75
2	25	922.434	1000	3	335		78
2	30	922.790	1000	3	335		80
2	35	922.910	1000	4	336		85
2	40	923.030	1000	5	334		87
1	45	923.149	1000	6	334		89
1	50	923.335	1000	6	335		90
1	55	923.525	1000	6	335		91
1	60	923.808	1000	6	330	↓	92
	$\theta = 60$	$V_m = 2.308$					$t_m = 81.75$

(0951)

$\sqrt{STD} = 2.163$

INTERPOLL LABORATORIES

Benzene Field Data Sheet

Job L.P. / Hayward, CA
 Source Line 2 / Keros / Stack
 Date 6-7-94 Test 20 Run 2

Operator(s) M. Kachler + K. Rosenthal
 Meter Box No. 55 Meter coef. 1.0015
 Barometric Pressure 28.73 in.Hg

Sample Train Leak Check:

Pretest: 0 cc/min at 16 in.Hg
 Posttest: 0 cc/min at 16 in.Hg

Trav. Point No.	Samp. Time (min)	Sample Volume (cf)	Sample Rate (cc/min)	VAC. (inHg)	Temperature (oF)		
					Stack	Probe	Gasmeter
	1142	924.800					
C-3	5	924.800	1000	3	335	NA	90
3	10	924.897	1000	3	337		91
3	15	925.173	1000	3	334		93
3	20	925.359	1000	3	334		95
2	25	925.545	1000	3	333		97
2	30	925.733	1000	3	337		99
2	35	925.920	1000	3	339		101
2	40	926.007	1000	3	339		103
1	45	926.123	1000	3	336		104
1	50	926.449	1000	3	336		107
1	55	926.669	1000	3	337		108
1	60	926.858	1000	3	337	↓	109
θ = 60		Vm = 2.258					tm = 99.75

(1242)

$$V_{STD} = 2.048$$

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INTERPOLL LABORATORIES

Benzene Field Data Sheet

Job L.P. / Hayward, WI
 Source Line 2 Kenos / Stack
 Date 6-7-94 Test 10 Run 3

Operator(s) M. Kachler & K. Rosenthal
 Meter Box No. 55 Meter coef. 1.0015
 Barometric Pressure 29.73 in.Hg

Sample Train Leak Check:

Pretest: 0 cc/min at 16 in.Hg

Posttest: 0 cc/min at 16 in.Hg

Trav. Point No.	Samp. Time (min)	Sample Volume (cf)	Sample Rate (cc/min)	VAC. (inHg)	Temperature (oF)		
					Stack	Probe	Gasmeter
	1436	926.90					
C-3	5	927.086	1000	3	337	NA	94
3	10	927.272	1000	3	336		94
3	15	927.457	1000	3	336		95
3	20	927.642	1000	3	340		97
2	25	927.835	1000	3	337		98
2	30	928.023	1000	3	338		99
2	35	928.210	1000	3	335		101
2	40	928.397	1000	3	337		102
1	45	928.584	1000	3	338		103
1	50	928.772	1000	3	332		104
1	55	928.956	1000	3	334		105
1	60	929.139	1000	3	335	↓	106
θ = 60		Vm = 2.239					tm = 99.83

(1536)

Vstd = 2.031

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APPENDIX E

INTERPOLL LABORATORIES ANALYTICAL DATA

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EPA Method 3 Data Reporting Sheet
Orsat Analysis

Job L.P. Howard Source Press RTO Outlet
Team Leader SB Test Site Stack
Date Submitted 6-13-94 Date of Test 6-7-94
Test No. 1 No. of Runs Completed 3
Date of Analysis 6-15-94 Technician C. Helgeson

Test/ Run	Sample Log Number and Type	No. of An.	Buret Readings (ml)			Conc. CO ₂ %v/v Dry	Conc. O ₂ %v/v Dry	F _o
			Zero Pt.	After CO ₂	After O ₂			
1/1	3097-101 ☒ B ☐ F	1	0.00	0.30	20.80	0.30	20.50	
		2	0.00	0.30	20.80	0.30	20.50	
		Avg				0.30	20.50	
1/2	-102 ☒ B ☐ F	1	0.00	0.40	20.90	0.40	20.50	
		2	0.00	0.40	20.90	0.40	20.50	
		Avg				0.40	20.50	
1/3	-103 ☒ B ☐ F	1	0.00	0.40	20.90	0.40	20.50	
		2	0.00	0.40	20.90	0.40	20.50	
		Avg				0.40	20.50	
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						

- ☒ Ambient Air QA Check
☒ Orsat Analyzer System Leak Check
☐ F_o Within EPA M-3 Guidelines for fuel type.

Where $F_o = \frac{20.9 - O_2}{CO_2}$

EPA Method 3 Guidelines

Fuel Type	F _o Range
Coal:	
Anthracite/Lignite	1.016-1.130
Bituminous	1.083-1.230
Oil:	
Distillate	1.260-1.413
Residual	1.210-1.370
Gas:	
Natural	1.600-1.836
Propane	1.434-1.586
Butane	1.405-1.553
Wood/Wood Bark	1.000-1.100

F=Flask (250 cc all glass)
B=Tedlar Bag (5-layer)

EPA Method 3 Data Reporting Sheet
Orsat Analysis

Job L.P. Hayward Source Press RTO outlet
Team Leader SB Test Site Stuck
Date Submitted 6-13-94 Date of Test 6-8-94
Test No. 2 No. of Runs Completed 3
Date of Analysis 6-15-94 Technician C. Helgeson

Test/ Run	Sample Log Number and Type	No. of An.	Buret Readings (ml)			Conc. CO ₂ %v/v Dry	Conc. O ₂ %v/v Dry	F _o
			Zero Pt.	After CO ₂	After O ₂			
2/1	3097-104 ☒ B ☐ F	1	0.00	0.40	21.00	0.40	20.60	
		2	0.00	0.40	21.00	0.40	20.60	
		Avg				0.40	20.60	
2/2	-105 ☒ B ☐ F	1	0.00	0.40	21.00	0.40	20.60	
		2	0.00	0.40	21.00	0.40	20.60	
		Avg				0.40	20.60	
2/3	-106 ☒ B ☐ F	1	0.00	0.40	21.00	0.40	20.60	
		2	0.00	0.40	21.00	0.40	20.60	
		Avg				0.40	20.60	
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						

- ☒ Ambient Air QA Check
☒ Orsat Analyzer System Leak Check
☐ F_o Within EPA M-3 Guidelines
for fuel type.

Where $F_o = \frac{20.9 - O_2}{CO_2}$

F=Flask (250 cc all glass)
B=Tedlar Bag (5-layer)

E-2

EPA Method 3 Guidelines	
Fuel Type	F _o Range
Coal:	
	Anthracite/Lignite 1.016-1.130
	Bituminous 1.083-1.230
Oil:	
	Distillate 1.260-1.413
	Residual 1.210-1.370
Gas:	
	Natural <u>other</u> 1.600-1.836
	Propane 1.434-1.586
	Butane 1.405-1.553
	Wood/Wood Bark 1.000-1.130

EPA Method 3 Data Reporting Sheet
Orsat Analysis

Job L.P. Hayward
Team Leader SB
Date Submitted 6-13-94
Test No. 3
Date of Analysis 6-15-94
Source Press RTO outlet
Test Site Stack
Date of Test 6-7-94
No. of Runs Completed 3
Technician C. Helgeson

Test/ Run	Sample Log Number and Type	No. of An.	Buret Readings (ml)			Conc. CO ₂	Conc. O ₂	F _o
			Zero Pt.	After CO ₂	After O ₂	%v/v Dry	%v/v Dry	
3/1	3097-113 B B F	1	0.00	0.40	20.90	0.40	20.50	
		2	0.00	0.40	20.90	0.40	20.50	
		Avg				0.40	20.50	
3/2	-114 B B F	1	0.00	0.40	20.90	0.40	20.50	
		2	0.00	0.40	20.90	0.40	20.50	
		Avg				0.40	20.50	
3/3	-115 B B F	1	0.00	0.40	20.90	0.40	20.50	
		2	0.00	0.40	20.90	0.40	20.50	
		Avg				0.40	20.50	
	B B F	1						
		2						
		Avg						
	B B F	1						
		2						
		Avg						
	B B F	1						
		2						
		Avg						
	B B F	1						
		2						
		Avg						
	B B F	1						
		2						
		Avg						
	B B F	1						
		2						
		Avg						
	B B F	1						
		2						
		Avg						

- ☐ Ambient Air QA Check
☐ Orsat Analyzer System Leak Check
☐ F_o Within EPA M-3 Guidelines
for fuel type.

Where $F_o = \frac{20.9 - O_2}{CO_2}$

F=Flask (250 cc all glass)
B=Tedlar Bag (5-layer)

EPA Method 3 Guidelines
F_o Range

Fuel Type	
Coal:	
Anthracite/Lignite	1.016-1.130
Bituminous	1.083-1.230
Oil:	
Distillate	1.260-1.413
Residual	1.210-1.370
Gas:	
Natural	1.600-1.836
Propane	1.434-1.586
Butane	1.405-1.553
Wood/Wood Bark	1.000-1.130

EPA Method 3 Data Reporting Sheet
Orsat Analysis

Job L. P. Hayward

Team Leader S.B.

Date Submitted 6-13-94

Test No. 3

Date of Analysis 6-18-94

Source # 1 Press RT0

Test Site outlet

Date of Test 6-10-94

No. of Runs Completed 3

Technician C. Helgeson

Test/ Run	Sample Log Number and Type	No. of An.	Buret Readings (ml)			Conc. CO ₂ %v/v Dry	Conc. O ₂ %v/v Dry	F _o
			Zero Pt.	After CO ₂	After O ₂			
3/1	3097-107 B B F	1	0.00	0.40	20.90	0.40	20.50	
		2	0.00	0.40	20.90	0.40	20.50	
		Avg				0.40	20.50	
3/2	-108 B B F	1	0.00	0.40	20.90	0.40	20.50	
		2	0.00	0.40	20.90	0.40	20.50	
		Avg				0.40	20.50	
3/3	-109 B B F	1	0.00	0.40	20.90	0.40	20.50	
		2	0.00	0.40	20.90	0.40	20.50	
		Avg				0.40	20.50	
	B B F	1						
		2						
		Avg						
	B B F	1						
		2						
		Avg						
	B B F	1						
		2						
		Avg						
	B B F	1						
		2						
		Avg						
	B B F	1						
		2						
		Avg						
	B B F	1						
		2						
		Avg						
	B B F	1						
		2						
		Avg						
	B B F	1						
		2						
		Avg						

- ☒ Ambient Air QA Check
☒ Orsat Analyzer System Leak Check
☐ F_o Within EPA M-3 Guidelines
for fuel type.

Where $F_o = \frac{20.9 - O_2}{CO_2}$

F=Flask (250 cc all glass)
B=Tedlar Bag (5-layer)

EPA Method 3 Guidelines
Fuel Type F_o Range

Coal:	
Anthracite/Lignite	1.016-1.130
Bituminous	1.083-1.230
Oil:	
Distillate	1.260-1.413
Residual	1.210-1.370
Gas:	
Natural	1.600-1.836
Propane	1.434-1.586
Butane	1.405-1.553
Wood/Wood Bark	1.000-1.130

EPA Method 3 Data Reporting Sheet
Orsat Analysis

Job L.P. Hayward Source Line 1 Konus
Team Leader ET Test Site Stack
Date Submitted 6-13-94 Date of Test 6-9-94
Test No. 6 No. of Runs Completed 3
Date of Analysis 6-15-94 Technician C. Helgeson

Test/ Run	Sample Log Number and Type	No. of An.	Buret Readings (ml)			Conc. CO ₂ %v/v Dry	Conc. O ₂ %v/v Dry	F _o
			Zero Pt.	After CO ₂	After O ₂			
6/1	3097-116 ☒ B ☐ F	1	0.00	6.20	20.70	6.20	14.50	1.03
		2	0.00	6.20	20.70	6.20	14.50	1.03
		Avg				6.20	14.50	
6/2	-117 ☒ B ☐ F	1	0.00	7.10	20.60	7.10	13.50	1.04
		2	0.00	7.10	20.60	7.10	13.50	1.04
		Avg				7.10	13.50	
6/3	-118 ☒ B ☐ F	1	0.00	6.50	20.70	6.50	14.20	1.03
		2	0.00	6.50	20.70	6.50	14.20	1.03
		Avg				6.50	14.20	
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						

- ☒ Ambient Air QA Check
☒ Orsat Analyzer System Leak Check
☐ F_o Within EPA M-3 Guidelines
for fuel type.

Where $F_o = \frac{20.9 - O_2}{CO_2}$

F=Flask (250 cc all glass)
B=Tedlar Bag (5-layer)

EPA Method 3 Guidelines	
Fuel Type	F _o Range
Coal:	
Anthracite/Lignite	1.016-1.130
Bituminous	1.083-1.230
Oil:	
Distillate	1.260-1.413
Residual	1.210-1.370
Gas:	
Natural	1.600-1.836
Propane	1.434-1.586
Butane	1.405-1.553
Wood/Wood	1.000-1.130

Bark

EPA Method 3 Data Reporting Sheet
Orsat Analysis

Job L.P. Hayward

Source Line 1 Konus

Team Leader MK

Test Site Stock

Date Submitted 6-13-94

Date of Test 6-9-94

Test No. 8

No. of Runs Completed 3

Date of Analysis 6-15-94

Technician C. Helgeson

Test/ Run	Sample Log Number and Type	No. of An.	Buret Readings (ml)			Conc. CO ₂ %v/v Dry	Conc. O ₂ %v/v Dry	F _o
			Zero Pt.	After CO ₂	After O ₂			
8/1	3097-119 ☐ B ☐ F	1	0.00	5.30	20.70	5.30	15.40	1.04
		2	0.00	5.30	20.70	5.30	15.40	1.04
		Avg				5.30	15.40	
8/2	-120 ☐ B ☐ F	1	0.00	5.90	20.80	5.90	14.90	1.02
		2	0.00	5.90	20.80	5.90	14.90	1.02
		Avg				5.90	14.90	
8/3	-121 ☐ B ☐ F	1	0.00	6.90	20.70	6.90	13.80	1.03
		2	0.00	6.90	20.70	6.90	13.80	1.03
		Avg				6.90	13.80	
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						

- ☒ Ambient Air QA Check
☒ Orsat Analyzer System Leak Check
☐ F_o Within EPA M-3 Guidelines
for fuel type.

Where F_o = $\frac{20.9 - O_2}{CO_2}$

F=Flask (250 cc all glass)
B=Tedlar Bag (5-layer)

EPA Method 3 Guidelines	
Fuel Type	F _o Range
Coal:	
Anthracite/Lignite	1.016-1.130
Bituminous	1.083-1.230
Oil:	
Distillate	1.260-1.413
Residual	1.210-1.370
Gas:	
Natural	1.600-1.836
Propane	1.434-1.586
Butane	1.405-1.553
Wood/Wood	1.000-1.130
	<u>Bark</u>

EPA Method 3 Data Reporting Sheet
Orsat AnalysisJob L.P. HaywardTeam Leader DUJ
Date Submitted 6-13-94
Test No. 12
Date of Analysis 6-15-94Source Line 2 Press Vent
Test Site RTO Stock
Date of Test 6-10-94
No. of Runs Completed 3
Technician C. Helgeson

Test/ Run	Sample Log Number and Type	No. of An.	Buret Readings (ml)			Conc. CO ₂ %v/v Dry	Conc. O ₂ %v/v Dry	F _o
			Zero Pt.	After CO ₂	After O ₂			
12/1	3097-125	1	0.00	0.40	21.00	0.40	20.60	
		2	0.00	0.40	20.90	0.40	20.50	
		Avg				0.40	20.55	
12/2	-126	1	0.00	0.40	21.00	0.40	20.60	
		2	0.00	0.40	21.00	0.40	20.60	
		Avg				0.40	20.60	
12/3	-127	1	0.00	0.40	21.00	0.40	20.60	
		2	0.00	0.40	20.90	0.40	20.50	
		Avg				0.40	20.55	
		1						
		2						
		Avg						
		1						
		2						
		Avg						
		1						
		2						
		Avg						
		1						
		2						
		Avg						
		1						
		2						
		Avg						
		1						
		2						
		Avg						
		1						
		2						
		Avg						

- ☐ Ambient Air QA Check
☒ Orsat Analyzer System Leak Check
☐ F_o Within EPA M-3 Guidelines
 for fuel type.

Where $F_o = \frac{20.9 - O_2}{CO_2}$

F=Flask (250 cc all glass)
 B=Tedlar Bag (5-layer)

EPA Method 3 Guidelines

Fuel Type	F _o Range
Coal:	
Anthracite/Lignite	1.016-1.130
Bituminous	1.083-1.230
Oil:	
Distillate	1.260-1.413
Residual	1.210-1.370
Gas:	
Natural	1.600-1.836
Propane	1.434-1.586
Butane	1.405-1.533
E-7 Wood/Wood Bark	1.000-1.130

Interpoll Laboratories
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EPA Method 3 Data Reporting Sheet
Orsat Analysis

Job L. P. Hayward

Team Leader DW

Date Submitted 6-13-94

Test No. 12

Date of Analysis 6-15-94

Source Line 2 Pres Vent

Test Site HSO Stack

Date of Test 6-8-94

No. of Runs Completed 7

Technician C. Helger

Test/ Run	Sample Log Number and Type	No. of An.	Buret Readings (ml)			Conc. CO ₂ %v/v Dry	Conc. O ₂ %v/v Dry	F _o
			Zero Pt.	After CO ₂	After O ₂			
12/1	3097-122 ☐ B ☐ F	1	0.00	0.30	20.90	0.30	20.60	
		2	0.00	0.30	20.90	0.30	20.60	
		Avg				0.30	20.60	
12/2	-123 ☐ B ☐ F	1	0.00	0.30	20.90	0.30	20.60	
		2	0.00	0.30	20.90	0.30	20.60	
		Avg				0.30	20.60	
12/3	-124 ☐ B ☐ F	1	0.00	0.30	20.90	0.30	20.60	
		2	0.00	0.30	20.90	0.30	20.60	
		Avg				0.30	20.60	
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						

- ☒ Ambient Air QA Check
☒ Orsat Analyzer System Leak Check
☐ F_o Within EPA M-3 Guidelines for fuel type.

Where $F_o = \frac{20.9 - O_2}{CO_2}$

EPA Method 3 Guidelines

Fuel Type	F _o Range
Coal:	
Anthracite/Lignite	1.016-1.130
Bituminous	1.083-1.230
Oil:	
Distillate	1.260-1.413
Residual	1.210-1.370
Gas:	
Natural	1.600-1.836
Propane	1.434-1.586
Butane	1.405-1.553
E-8 Wood/Wood Bark	1.000-1.130

F=Flask (250 cc all glass)
B=Tedlar Bag (5-layer)

EPA Method 3 Data Reporting Sheet
Orsat Analysis

Job L.P. Hayward Source Line 2 Press
Team Leader J Test Site RTO stack
Date Submitted 6-13-94 Date of Test 6-9-94
Test No. 14 No. of Runs Completed 3
Date of Analysis 6-15-94 Technician C. Helgeson

Test/ Run	Sample Log Number and Type	No. of An.	Buret Readings (ml)			Conc. CO ₂ %v/v Dry	Conc. O ₂ %v/v Dry	F _o
			Zero Pt.	After CO ₂	After O ₂			
14/1	3097-128 B F	1	0.00	0.40	21.00	0.40	20.60	
		2	0.00	0.40	21.00	0.40	20.60	
		Avg				0.40	20.60	
14/2	-129 B F	1	0.00	0.40	21.00	0.40	20.60	
		2	0.00	0.40	21.00	0.40	20.60	
		Avg				0.40	20.60	
14/3	-130 B F	1	0.00	0.40	21.00	0.40	20.60	
		2	0.00	0.40	20.90	0.40	20.50	
		Avg				0.40	20.55	
	B F	1						
		2						
		Avg						
	B F	1						
		2						
		Avg						
	B F	1						
		2						
		Avg						
	B F	1						
		2						
		Avg						
	B F	1						
		2						
		Avg						
	B F	1						
		2						
		Avg						
	B F	1						
		2						
		Avg						

- ☒ Ambient Air QA Check
☐ Orsat Analyzer System Leak Check
☐ F_o Within EPA M-3 Guidelines
for fuel type.

Where $F_o = 20.9 - O_2$
CO₂

F=Flask (250 cc all glass)
B=Tedlar Bag (5-layer)

EPA Method 3 Guidelines	
Fuel Type	F _o Range
Coal:	
Anthracite/Lignite	1.016-1.130
Bituminous	1.083-1.230
Oil:	
Distillate	1.260-1.413
Residual	1.210-1.370
Gas:	
Natural	1.600-1.836
Propane	1.434-1.586
Butane	1.405-1.553
Wood/Wood Bark	1.000-1.130

EPA Method 3 Data Reporting Sheet
Orsat AnalysisJob L.P. HaywardTeam Leader JMKDate Submitted 6-13-94Test No. 17, 18Date of Analysis 6-15-94Source Line 2 KongsTest Site StackDate of Test 6-8-94No. of Runs Completed 3Technician C. Helgeson

Test/ Run	Sample Log Number and Type	No. of An.	Buret Readings (ml)			Conc. CO ₂ %v/v Dry	Conc. O ₂ %v/v Dry	F _o
			Zero Pt.	After CO ₂	After O ₂			
17 ¹⁸ / 1	3097- B B F	1	0.00	4.40	21.00	4.40	16.60	1.00
		2	0.00	4.40	21.00	4.40	16.60	1.00
		Avg				4.40	16.60	
17 ¹⁸ / 2	-131 B B F	1	0.00	4.40	21.00	4.40	16.60	1.00
		2	0.00	4.40	21.00	4.40	16.60	1.00
		Avg				4.40	16.60	
17 ¹⁸ / 3	-132 B B F	1	0.00	4.30	20.90	4.30	16.60	1.00
		2	0.00	4.30	20.90	4.30	16.60	1.00
		Avg				4.30	16.60	
	B B F	1						
		2						
		Avg						
	B B F	1						
		2						
		Avg						
	B B F	1						
		2						
		Avg						
	B B F	1						
		2						
		Avg						
	B B F	1						
		2						
		Avg						
	B B F	1						
		2						
		Avg						
	B B F	1						
		2						
		Avg						

- ☒ Ambient Air QA Check
☒ Orsat Analyzer System Leak Check
☐ F_o Within EPA M-3 Guidelines
 for fuel type.

Where $F_o = \frac{20.9 - O_2}{CO_2}$

F=Flask (250 cc all glass)
 B=Tedlar Bag (5-layer)

EPA Method 3 Guidelines

Fuel Type	F _o Range
Coal:	
Anthracite/Lignite	1.016-1.130
Bituminous	1.083-1.230
Oil:	
Distillate	1.260-1.413
Residual	1.210-1.370
Gas:	
Natural	1.600-1.836
Propane	1.434-1.586
Butane	1.405-1.553
Wood/Wood	1.000-1.130

E-10 Wood/Wood Bark

LSC-04-RR

EPA Method 3 Data Reporting Sheet
Orsat Analysis

Job L.P. Hayward

Team Leader MK
Date Submitted 6-13-94
Test No. 19
Date of Analysis 6-15-94

Source Line 2 Konus
Test Site Stack
Date of Test 6-7-94
No. of Runs Completed 3
Technician C. Helgeson

Test/ Run	Sample Log Number and Type	No. of An.	Buret Readings (ml)			Conc. CO ₂ %v/v Dry	Conc. O ₂ %v/v Dry	F _o
			Zero Pt.	After CO ₂	After O ₂			
19/1	3091-133 ☒ B ☐ F	1	0.00	5.00	20.80	5.00	15.80	1.02
		2	0.00	5.00	20.80	5.00	15.80	1.02
		Avg				5.00	15.80	
19/2	-134 ☒ B ☐ F	1	0.00	4.90	20.80	4.90	15.90	1.02
		2	0.00	4.90	20.80	4.90	15.90	1.02
		Avg				4.90	15.90	
19/3	-135 ☒ B ☐ F	1	0.00	4.00	20.90	4.00	16.90	1.00
		2	0.00	4.00	20.90	4.00	16.90	1.00
		Avg				4.00	16.90	
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						

- ☒ Ambient Air QA Check
☒ Orsat Analyzer System Leak Check
☐ F_o Within EPA M-3 Guidelines
for fuel type.

Where $F_o = \frac{20.9 - O_2}{CO_2}$

F=Flask (250 cc all glass)
B=Tedlar Bag (5-layer)

EPA Method 3 Guidelines

Fuel Type	F _o Range
Coal:	
Anthracite/Lignite	1.016-1.130
Bituminous	1.083-1.230
Oil:	
Distillate	1.260-1.413
Residual	1.210-1.370
Gas:	
Natural	1.600-1.836
Propane	1.434-1.586
Butane	1.405-1.553
Wood/Wood <u>Bark</u>	1.000-1.130

EPA Method 5 Data Reporting Sheet
Impinger Catch/Wisconsin Protocol

Job LP. Hayward Source Live 1 Press RTO
Team Leader MK Test Site Inlet
Date Submitted 6-13-94 Date of Test 6-10-94
Test No. 5 No. of Runs Completed 3
Date of Analysis 6-29-94 Technician C. Helgeson

		Solvent Phase	Aqueous Phase
0	Test <u>Run 0</u> Field Blank Log Number Comments	Dish No. Dish Tare Wt. <u>g</u> Dish+Sample Wt. <u>g</u> Sample Wt. <u>g</u>	Dish No. Dish Tare Wt. <u>g</u> Dish+Sample Wt. <u>g</u> Sample Wt. <u>g</u>
1	Test <u>5</u> Run <u>1</u> Log Number <u>3097-1712</u> Comments	Dish No. <u>105</u> Dish Tare Wt. <u>47.8630</u> g Dish+Sample Wt. <u>47.8664</u> g Sample Wt. <u>0.0034</u> g	Dish No. <u>35</u> Dish Tare Wt. <u>51.0908</u> g Dish+Sample Wt. <u>51.1052</u> g Sample Wt. <u>0.0144</u> g
2	Test <u>5</u> Run <u>2</u> Log Number <u>1722</u> Comments	Dish No. <u>520</u> Dish Tare Wt. <u>48.5275</u> g Dish+Sample Wt. <u>48.5310</u> g Sample Wt. <u>0.0035</u> g	Dish No. <u>312</u> Dish Tare Wt. <u>45.2347</u> g Dish+Sample Wt. <u>45.2475</u> g Sample Wt. <u>0.0128</u> g
3	Test <u>5</u> Run <u>3</u> Log Number <u>1733</u> Comments	Dish No. <u>521</u> Dish Tare Wt. <u>50.5981</u> g Dish+Sample Wt. <u>50.5992</u> g Sample Wt. <u>0.0011</u> g	Dish No. <u>403</u> Dish Tare Wt. <u>47.0941</u> g Dish+Sample Wt. <u>47.1077</u> g Sample Wt. <u>0.0136</u> g
4	Test <u>Run</u> Log Number Comments	Dish No. Dish Tare Wt. <u>g</u> Dish+Sample Wt. <u>g</u> Sample Wt. <u>g</u>	Dish No. Dish Tare Wt. <u>g</u> Dish+Sample Wt. <u>g</u> Sample Wt. <u>g</u>
5	Test <u>Run</u> Log Number Comments	Dish No. Dish Tare Wt. <u>g</u> Dish+Sample Wt. <u>g</u> Sample Wt. <u>g</u>	Dish No. Dish Tare Wt. <u>g</u> Dish+Sample Wt. <u>g</u> Sample Wt. <u>g</u>

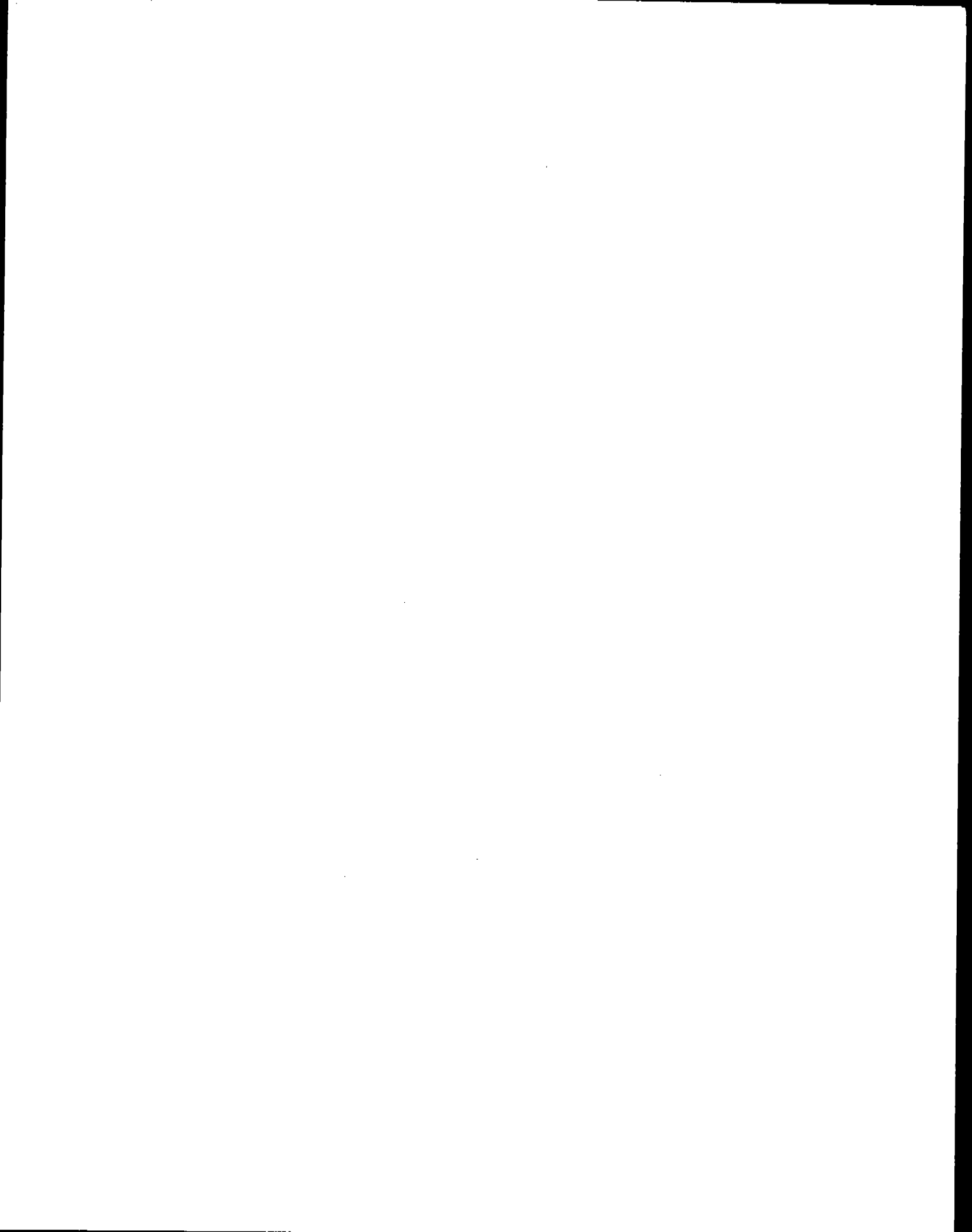
Results Solvent Phase:

Field Blk.	Run 1	Run 2	Run 3	Run 4	Run 5
	<u>0.0030</u>	<u>0.0031</u>	<u>0.0007</u>		

Results Aqueous Phase:

Field Blk.	Run 1	Run 2	Run 3	Run 4	Run 5
	<u>0.0141</u>	<u>0.0125</u>	<u>0.0133</u>		<u>E-12</u>

LSC-03WYR



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EPA Method 5 Data Reporting Sheet
Probe/Cyclone Wash

Job L.P. Hayward Source Live | Press RTO
Team Leader MK Test Site Inlet
Date Submitted 6-13-94 Date of Test 6-10-94
Test No. 5 No. of Runs Completed 3
Date of Analysis 6-10-94 Technician C. Helgeson
Transport Leakage ☒ None ☐ ml Solvent Acetone

0	Test <u> </u> Run <u>0</u> Field Blank Log Number <u> </u> Vol. of Solvent <u> </u> ml *Solvent Residue <u>3.0</u> ug/ml	Dish No. <u> </u> Dish Tare Wt. <u> </u> g Dish+Sample Wt. <u> </u> g Sample Wt. <u> </u> g
1	Test <u>5</u> Run <u>1</u> Vol. of Solvent <u>100</u> ml Log Number <u>3097-171P</u> Comments <u> </u>	Dish No. <u>52</u> Dish Tare Wt. <u>49.8058</u> g Dish+Sample Wt. <u>49.8222</u> g Sample Wt. <u>0.0164</u> g
2	Test <u>5</u> Run <u>2</u> Vol. of Solvent <u>160</u> ml Log Number <u>-172P</u> Comments <u> </u>	Dish No. <u>55</u> Dish Tare Wt. <u>47.7784</u> g Dish+Sample Wt. <u>47.7914</u> g Sample Wt. <u>0.0130</u> g
3	Test <u>5</u> Run <u>3</u> Vol. of Solvent <u>140</u> ml Log Number <u>-173P</u> Comments <u> </u>	Dish No. <u>62</u> Dish Tare Wt. <u>50.8877</u> g Dish+Sample Wt. <u>50.9002</u> g Sample Wt. <u>0.0125</u> g
4	Test <u> </u> Run <u> </u> Vol. of Solvent <u> </u> ml Log Number <u> </u> Comments <u> </u>	Dish No. <u> </u> Dish Tare Wt. <u> </u> g Dish+Sample Wt. <u> </u> g Sample Wt. <u> </u> g
5	Test <u> </u> Run <u> </u> Vol. of Solvent <u> </u> ml Log Number <u> </u> Comments <u> </u>	Dish No. <u> </u> Dish Tare Wt. <u> </u> g Dish+Sample Wt. <u> </u> g Sample Wt. <u> </u> g

*Solvent Residue ug/ml = ((Sample Wt. g) (10⁶) / Vol. of Sol. ml)
EPA-MS Acetone Residue Blank Spec. { 7.3 ug/ml

Results:
Field Blk. Run 1 Run 2 Run 3 Run 4 Run 5

	0.0161	0.0125	0.0121		E-13
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SC-01190

EPA Method 5 Data Reporting Sheet
Filter Gravimetrics

Job L.P. Hayward Source Line 1 Press RTO
Team Leader MK Test Site Inlet
Date Submitted _____ Date of Test 6-10-94
Test No. 5 No. of Runs Completed 3
Date of Analysis 6-29-94 Technician C. Helgeson

0	Test <u>Run 0</u> Field Blank Log Number _____ Comments _____	Filter No. _____ Filter Type _____ Filter Tare Wt. _____ g Filter+Sample Wt. _____ g Sample Wt. _____ g
1	Test <u>5</u> Run <u>1</u> Log Number <u>3097-171F</u> Comments _____	Filter No. <u>1318</u> Filter Type <u>3.52 Pallflex</u> Filter Tare Wt. <u>.3582</u> g Filter+Sample Wt. <u>.3680</u> g Sample Wt. <u>0.0098</u> g
2	Test <u>5</u> Run <u>2</u> Log Number <u>172F</u> Comments _____	Filter No. <u>1319</u> Filter Type <u>3.52 Pallflex</u> Filter Tare Wt. <u>.3588</u> g Filter+Sample Wt. <u>.3602</u> g Sample Wt. <u>0.0014</u> g
3	Test <u>5</u> Run <u>3</u> Log Number <u>173F</u> Comments _____	Filter No. <u>1320</u> Filter Type <u>3.52 Pallflex</u> Filter Tare Wt. <u>.3516</u> g Filter+Sample Wt. <u>.3642</u> g Sample Wt. <u>0.0126</u> g
4	Test _____ Run _____ Log Number _____ Comments _____	Filter No. _____ Filter Type _____ Filter Tare Wt. _____ g Filter+Sample Wt. _____ g Sample Wt. _____ g
5	Test _____ Run _____ Log Number _____ Comments _____	Filter No. _____ Filter Type _____ Filter Tare Wt. _____ g Filter+Sample Wt. _____ g Sample Wt. _____ g

Results:

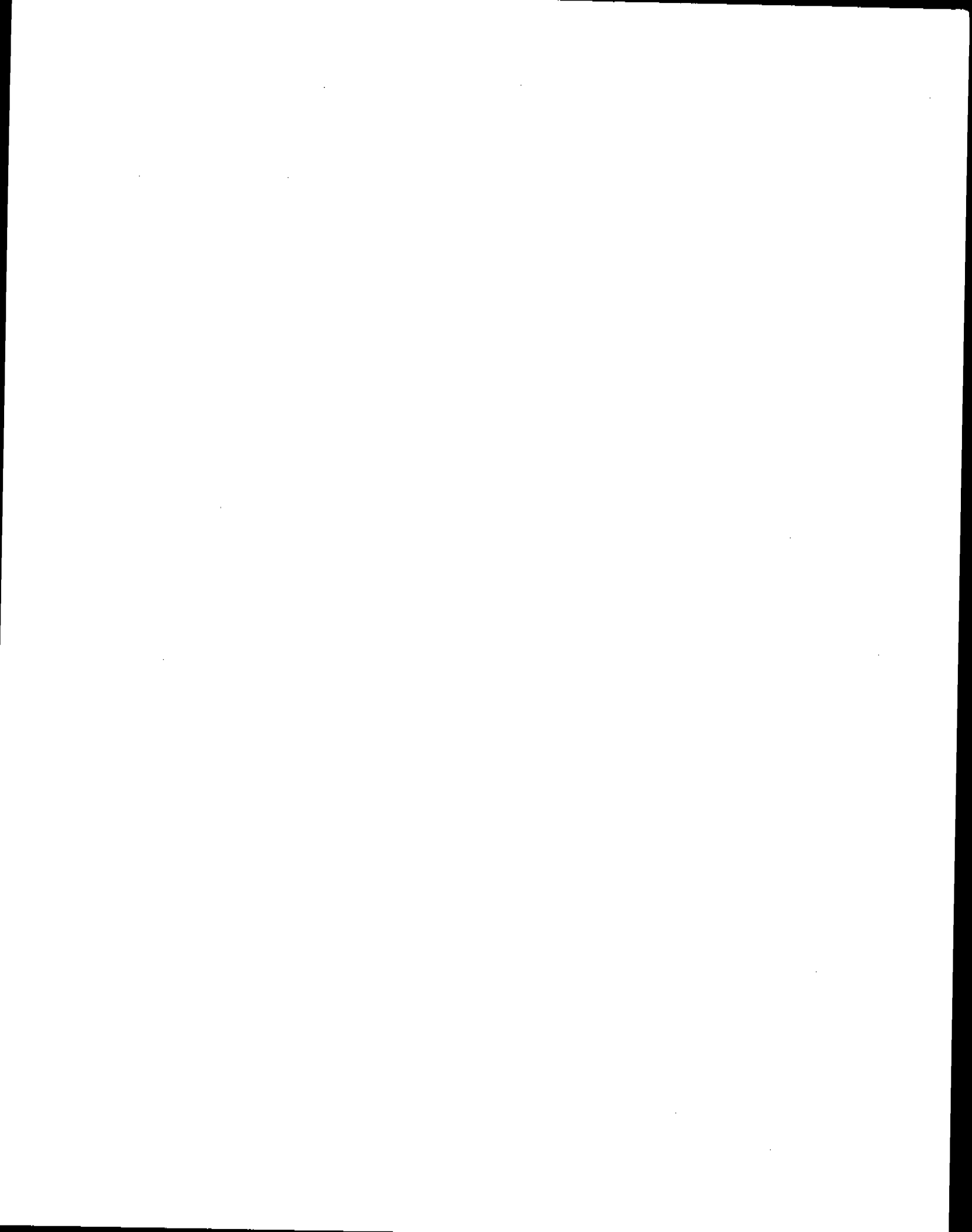
Field Blk. Run 1 Run 2 Run 3 Run 4 Run 5

	0.0098	0.0014	0.0126		
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Field Blk. Run 1 Run 2 Run 3 Run 4 Run 5

	0.0430	0.0295	0.0387		
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LSC-02PR



EPA Method 5 Data Reporting Sheet
Impinger Catch/Wisconsin Protocol

Job L.P. Hayward Source #1 Press RTO
Team Leader SB Test Site Outlet
Date Submitted 6-13-94 Date of Test 6-10-94
Test No. 3 No. of Runs Completed 3
Date of Analysis 6-29-94 Technician C. Nelson

	Solvent Phase	Aqueous Phase
0	Test <u>Run 0</u> Field Blank Log Number Comments	Dish No. _____ Dish Tare Wt. _____ g Dish+Sample Wt. _____ g Sample Wt. _____ g
1	Test <u>3</u> Run <u>1</u> Log Number <u>3097-1605</u> Comments	Dish No. <u>328</u> Dish Tare Wt. <u>41.9670</u> g Dish+Sample Wt. <u>41.9699</u> g Sample Wt. <u>0.0029</u> g
2	Test <u>3</u> Run <u>2</u> Log Number <u>-1612</u> Comments	Dish No. <u>404</u> Dish Tare Wt. <u>47.6374</u> g Dish+Sample Wt. <u>47.6520</u> g Sample Wt. <u>0.0146</u> g
3	Test <u>3</u> Run <u>3</u> Log Number <u>-1625</u> Comments	Dish No. <u>415</u> Dish Tare Wt. <u>45.0805</u> g Dish+Sample Wt. <u>45.0884</u> g Sample Wt. <u>0.0079</u> g
4	Test <u>Run</u> Log Number Comments	Dish No. _____ Dish Tare Wt. _____ g Dish+Sample Wt. _____ g Sample Wt. _____ g
5	Test <u>Run</u> Log Number Comments	Dish No. _____ Dish Tare Wt. _____ g Dish+Sample Wt. _____ g Sample Wt. _____ g

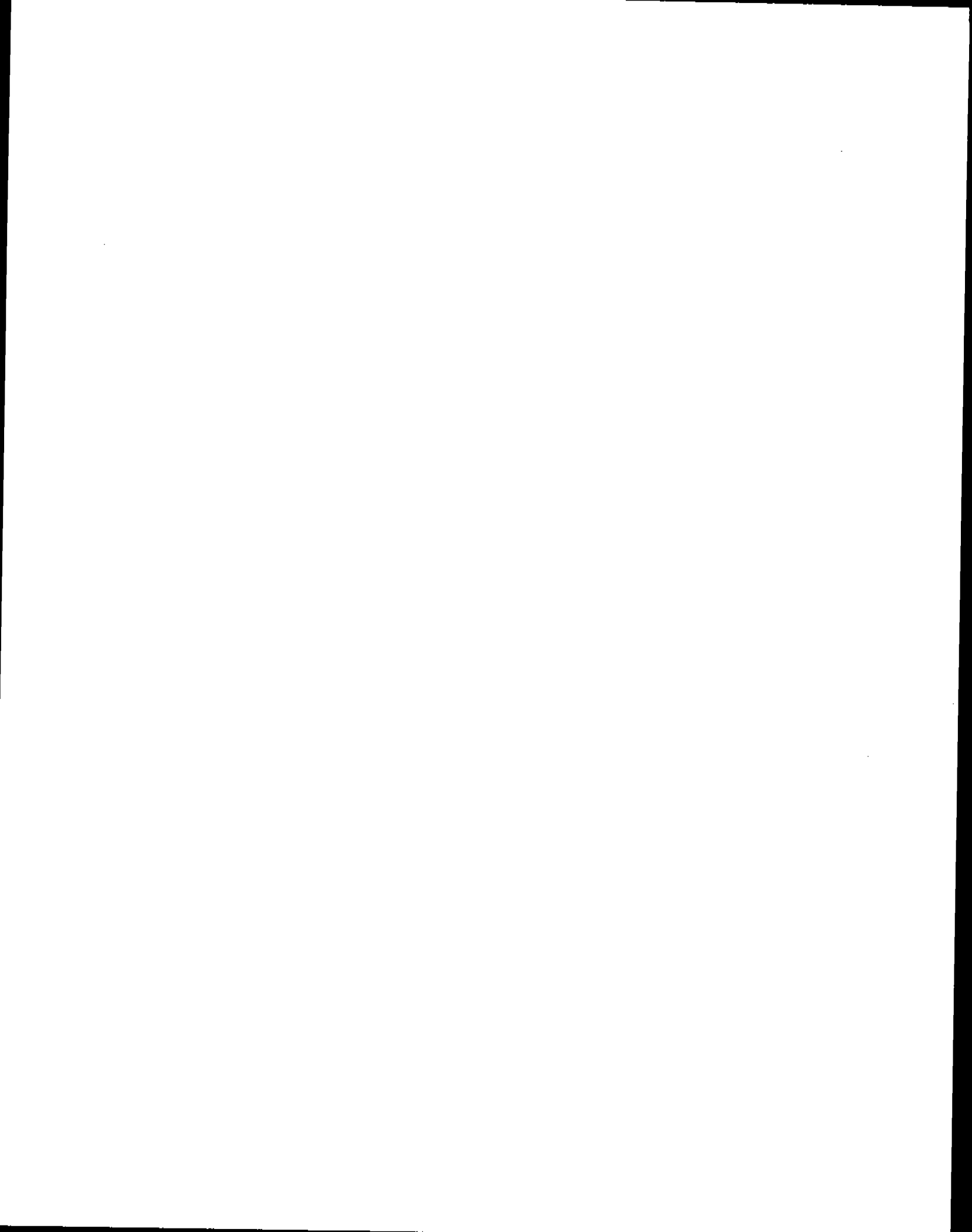
Results Solvent Phase:

Field Blk.	Run 1	Run 2	Run 3	Run 4	Run 5
	<u>0.0025</u>	<u>0.0036</u>	<u>0.0054</u>		

Results Aqueous Phase:

Field Blk.	Run 1	Run 2	Run 3	Run 4	Run 5
	<u>0.0112</u>	<u>0.0143</u>	<u>0.0076</u>		<u>E-15</u>

LSC-03WYR



EPA Method 5 Data Reporting Sheet
Probe/Cyclone Wash

Job L.P. Hayward Source #1 Press RTO
Team Leader SB Test Site Outlet
Date Submitted 6-13-94 Date of Test 6-10-94
Test No. 3 No. of Runs Completed 3
Date of Analysis 6-30-94 Technician C. Helgeson
Transport Leakage ☒ None ☐ ml Solvent Acetone

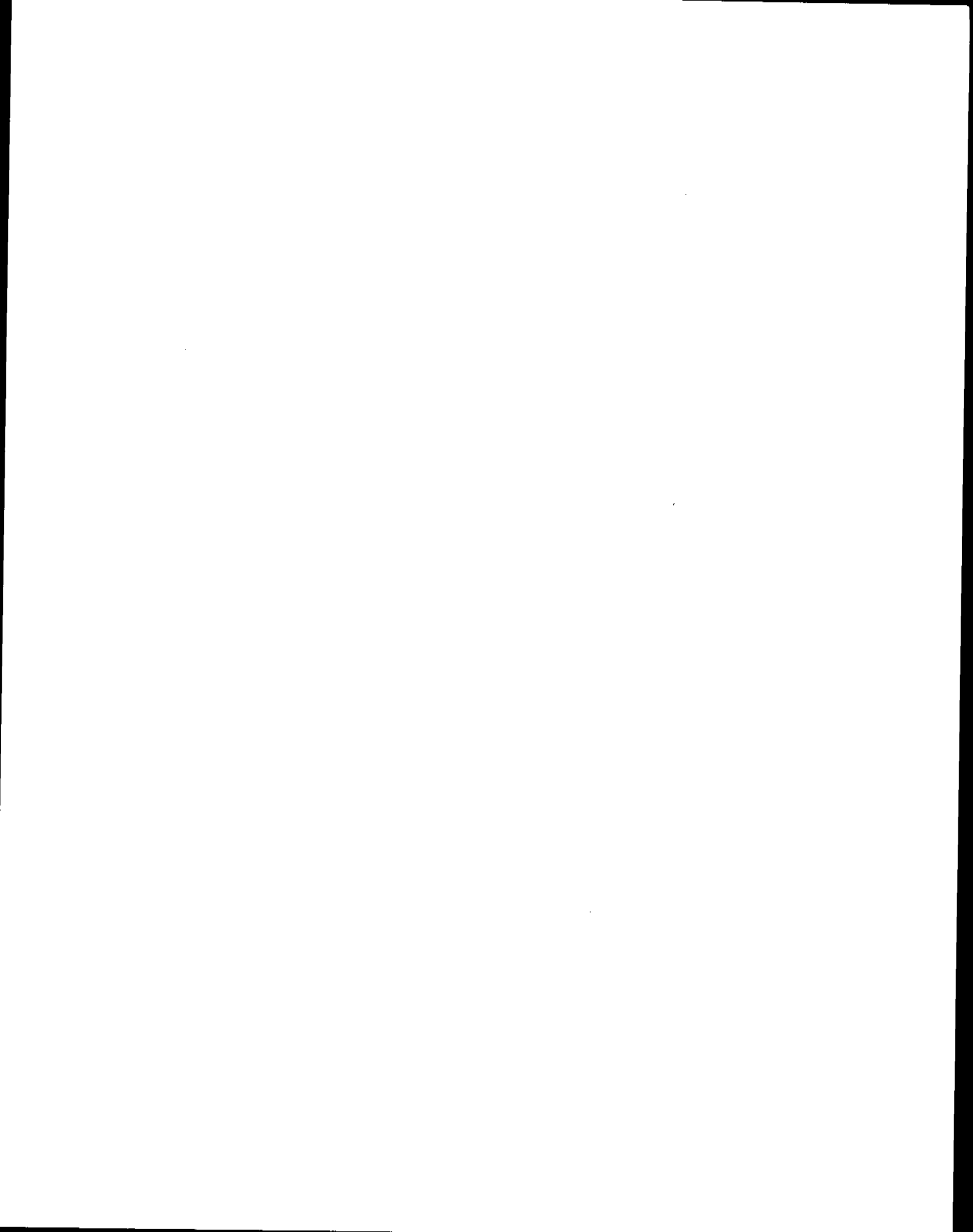
0	Test <u>Run 3</u> Field Blank Log Number <u> </u> Vol. of Solvent <u> </u> ml *Solvent Residue <u>3.0</u> ug/ml	Dish No. <u> </u> Dish Tare Wt. <u> </u> g Dish+Sample Wt. <u> </u> g Sample Wt. <u> </u> g
1	Test <u>3</u> Run <u>1</u> Vol. of Solvent <u>90</u> ml Log Number <u>3097-160P</u> Comments <u> </u>	Dish No. <u>40</u> Dish Tare Wt. <u>47.6416</u> g Dish+Sample Wt. <u>47.6585</u> g Sample Wt. <u>0.0169</u> g
2	Test <u>3</u> Run <u>2</u> Vol. of Solvent <u>80</u> ml Log Number <u>161P</u> Comments <u> </u>	Dish No. <u>43</u> Dish Tare Wt. <u>47.3874</u> g Dish+Sample Wt. <u>47.3939</u> g Sample Wt. <u>0.0065</u> g
3	Test <u>3</u> Run <u>3</u> Vol. of Solvent <u>50</u> ml Log Number <u>162P</u> Comments <u> </u>	Dish No. <u>59</u> Dish Tare Wt. <u>44.7327</u> g Dish+Sample Wt. <u>44.7381</u> g Sample Wt. <u>0.0054</u> g
4	Test <u> </u> Run <u> </u> Vol. of Solvent <u> </u> ml Log Number <u> </u> Comments <u> </u>	Dish No. <u> </u> Dish Tare Wt. <u> </u> g Dish+Sample Wt. <u> </u> g Sample Wt. <u> </u> g
5	Test <u> </u> Run <u> </u> Vol. of Solvent <u> </u> ml Log Number <u> </u> Comments <u> </u>	Dish No. <u> </u> Dish Tare Wt. <u> </u> g Dish+Sample Wt. <u> </u> g Sample Wt. <u> </u> g

*Solvent Residue ug/ml = [(Sample Wt. g) (10⁶) / Vol. of Sol. ml]
EPA-MS Acetone Residue Blank Spec. { 7.3 ug/ml

Results:

	Run 1	Run 2	Run 3	Run 4	Run 5
Field Blk.	0.0166	0.0063	0.0052		E-16

LSC-01YR



EPA Method 5 Data Reporting Sheet
Filter Gravimetrics

Job L.P. Hayward WI Source #1 Press RTO
Team Leader SB Test Site Outlet
Date Submitted 6-13-94 Date of Test 6-10-94
Test No. 3 No. of Runs Completed 3
Date of Analysis 6-27-94 Technician C. Halgeson

0	Test <u>Run 0</u> Field Blank Log Number _____ Comments _____	Filter No. _____ Filter Type _____ Filter Tare Wt. _____ g Filter+Sample Wt. _____ g Sample Wt. _____ g
1	Test <u>3</u> Run <u>1</u> Log Number <u>3097-160F</u> Comments _____	Filter No. <u>4041</u> Filter Type <u>4" Pallflex</u> Filter Tare Wt. <u>0.6264</u> g Filter+Sample Wt. <u>0.6272</u> g Sample Wt. <u>0.0008</u> g
2	Test <u>3</u> Run <u>2</u> Log Number <u>161F</u> Comments _____	Filter No. <u>4044</u> Filter Type <u>4" Pallflex</u> Filter Tare Wt. <u>0.6254</u> g Filter+Sample Wt. <u>0.6282</u> g Sample Wt. <u>0.0028</u> g
3	Test <u>3</u> Run <u>3</u> Log Number <u>162F</u> Comments _____	Filter No. <u>4043</u> Filter Type <u>4" Pallflex</u> Filter Tare Wt. <u>0.6324</u> g Filter+Sample Wt. <u>0.6363</u> g Sample Wt. <u>0.0039</u> g
4	Test <u>Run</u> Log Number _____ Comments _____	Filter No. _____ Filter Type _____ Filter Tare Wt. _____ g Filter+Sample Wt. _____ g Sample Wt. _____ g
5	Test <u>Run</u> Log Number _____ Comments _____	Filter No. _____ Filter Type _____ Filter Tare Wt. _____ g Filter+Sample Wt. _____ g Sample Wt. _____ g

Results:

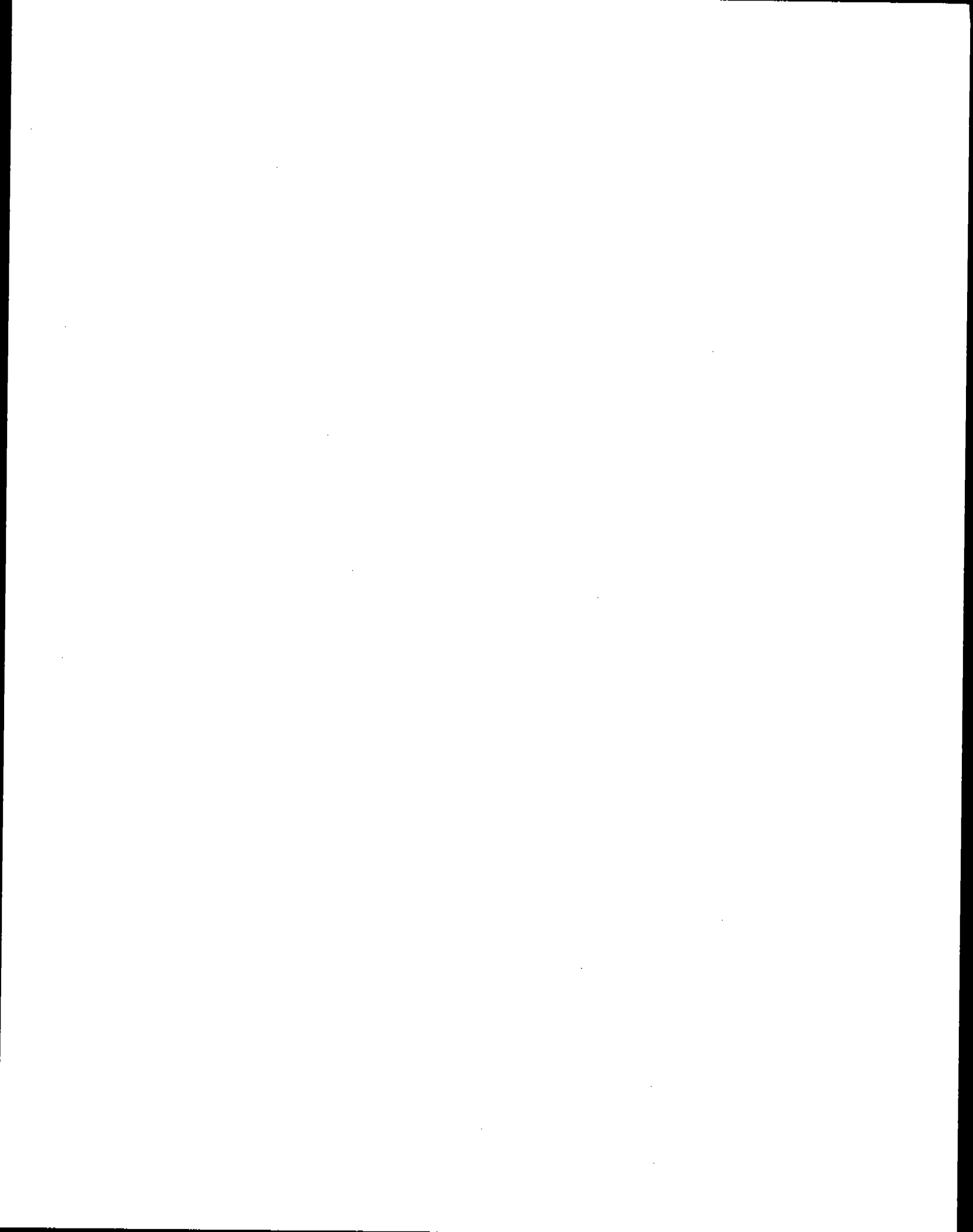
Field Blk. Run 1 Run 2 Run 3 Run 4 Run 5

	0.0008	0.0028	0.0039		
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Field Blk. Run 1 Run 2 Run 3 Run 4 Run 5

	0.0311	0.0270	0.0275		
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LSC-02PR



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EPA Method 5 Data Reporting Sheet
Impinger Catch/Wisconsin Protocol

o L.P. Hayward Source Press RTO
Team Leader SB Test Site Inlet
Date Submitted 6-13-94 Date of Test 6-7-94
Test No. 21 No. of Runs Completed 3
Date of Analysis 6-30-94 Technician C. Hakeson

	Solvent Phase	Aqueous Phase
Test <u>Run 0</u> Field Blank Log Number _____ Comments _____	Dish No. _____ Dish Tare Wt. _____ g Dish+Sample Wt. _____ g Sample Wt. _____ g	Dish No. _____ Dish Tare Wt. _____ g Dish+Sample Wt. _____ g Sample Wt. _____ g
Test <u>21</u> Run <u>1</u> Log Number <u>3097-1821</u> Comments _____	Dish No. <u>400</u> Dish Tare Wt. <u>47.0994</u> g Dish+Sample Wt. <u>47.1038</u> g Sample Wt. <u>0.0044</u> g	Dish No. <u>13</u> Dish Tare Wt. <u>45.7202</u> g Dish+Sample Wt. <u>45.7274</u> g Sample Wt. <u>0.0072</u> g
Test <u>21</u> Run <u>2</u> Log Number <u>-1831</u> Comments _____	Dish No. <u>401</u> Dish Tare Wt. <u>49.5238</u> g Dish+Sample Wt. <u>49.5283</u> g Sample Wt. <u>0.0045</u> g	Dish No. <u>518</u> Dish Tare Wt. <u>48.1017</u> g Dish+Sample Wt. <u>48.1341</u> g Sample Wt. <u>0.0324</u> g
Test <u>21</u> Run <u>3</u> Log Number <u>-1841</u> Comments _____	Dish No. <u>409</u> Dish Tare Wt. <u>46.1890</u> g Dish+Sample Wt. <u>46.1937</u> g Sample Wt. <u>0.0047</u> g	Dish No. <u>619</u> Dish Tare Wt. <u>47.5523</u> g Dish+Sample Wt. <u>47.5568</u> g Sample Wt. <u>0.0045</u> g
Test <u>Run</u> Log Number _____ Comments _____	Dish No. _____ Dish Tare Wt. _____ g Dish+Sample Wt. _____ g Sample Wt. _____ g	Dish No. _____ Dish Tare Wt. _____ g Dish+Sample Wt. _____ g Sample Wt. _____ g
Test <u>Run</u> Log Number _____ Comments _____	Dish No. _____ Dish Tare Wt. _____ g Dish+Sample Wt. _____ g Sample Wt. _____ g	Dish No. _____ Dish Tare Wt. _____ g Dish+Sample Wt. _____ g Sample Wt. _____ g

Results Solvent Phases:

Field Blk.	Run 1	Run 2	Run 3	Run 4	Run 5
	0.0040	0.0041	0.0043		

Results Aqueous Phases:

Field Blk.	Run 1	Run 2	Run 3	Run 4	Run 5
	0.0068	0.0321	0.0041		E-18

LSC-03WYR

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EPA Method 5 Data Reporting Sheet
Probe/Cyclone Wash

Job L.P. Hayward Source Press RTO #2
Team Leader SB Test Site Inlet
Date Submitted 6-13-94 Date of Test 6-9-94
Test No. 21 No. of Runs Completed 3
Date of Analysis 6-30-94 Technician C. Helgeson
Transport Leakage ☒ None ml Solvent Acetone

3	Test <u>Run 0</u> Field Blank Log Number _____ Vol. of Solvent _____ ml *Solvent Residue <u>3.0</u> ug/ml	Dish No. _____ Dish Tare Wt. _____ g Dish+Sample Wt. _____ g Sample Wt. _____ g
1	Test <u>21</u> Run <u>1</u> Vol. of Solvent <u>100</u> ml Log Number <u>3047-182P</u> Comments _____	Dish No. <u>29</u> Dish Tare Wt. <u>48.8864</u> g Dish+Sample Wt. <u>49.1088</u> g Sample Wt. <u>0.2224</u> g
2	Test <u>21</u> Run <u>2</u> Vol. of Solvent <u>110</u> ml Log Number <u>-183P</u> Comments _____	Dish No. <u>212</u> Dish Tare Wt. <u>50.3551</u> g Dish+Sample Wt. <u>50.4611</u> g Sample Wt. <u>0.1060</u> g
3	Test <u>21</u> Run <u>3</u> Vol. of Solvent <u>120</u> ml Log Number <u>-184P</u> Comments _____	Dish No. <u>306</u> Dish Tare Wt. <u>42.8341</u> g Dish+Sample Wt. <u>42.9102</u> g Sample Wt. <u>0.0761</u> g
4	Test _____ Run _____ Vol. of Solvent _____ ml Log Number _____ Comments _____	Dish No. _____ Dish Tare Wt. _____ g Dish+Sample Wt. _____ g Sample Wt. _____ g
5	Test _____ Run _____ Vol. of Solvent _____ ml Log Number _____ Comments _____	Dish No. _____ Dish Tare Wt. _____ g Dish+Sample Wt. _____ g Sample Wt. _____ g

*Solvent Residue _____ ug/ml = [(Sample Wt. _____ g) (10⁶)] / Vol. of Sol. _____ ml
EPA-MS Acetone Residue Blank Spec. (7.3 ug/ml)

Results:

Field Blk. Run 1 Run 2 Run 3 Run 4 Run 5

	0.2221	0.1057	0.0757		E-19
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15C-01V9

EPA Method 5 Data Reporting Sheet
Filter Gravimetrics

Job L.P. Hayward Source #2 Press RTO
Team Leader SB Test Site Inlet
Date Submitted 6-13-94 Date of Test 6-9-94
Test No. 21 No. of Runs Completed 3
Date of Analysis 6-29-94 Technician C. Helgeson

0	Test <u>Run 0</u> Field Blank Log Number _____ Comments _____	Filter No. _____ Filter Type _____ Filter Tare Wt. _____ g Filter+Sample Wt. _____ g Sample Wt. _____ g
1	Test <u>21</u> Run <u>1</u> Log Number <u>3097-182F</u> Comments _____	Filter No. <u>1315</u> Filter Type <u>3.52 Pallflex</u> Filter Tare Wt. <u>.3566</u> g Filter+Sample Wt. <u>.5920</u> g Sample Wt. <u>0.2354</u> g
2	Test <u>21</u> Run <u>2</u> Log Number <u>-183F</u> Comments _____	Filter No. <u>1316</u> Filter Type <u>3.52 Pallflex</u> Filter Tare Wt. <u>.3647</u> g Filter+Sample Wt. <u>.5501</u> g Sample Wt. <u>0.1854</u> g
3	Test <u>21</u> Run <u>3</u> Log Number <u>-184F</u> Comments _____	Filter No. <u>1317</u> Filter Type <u>3.52 Pallflex</u> Filter Tare Wt. <u>.3639</u> g Filter+Sample Wt. <u>.7150</u> g Sample Wt. <u>0.3511</u> g
4	Test <u>Run</u> Log Number _____ Comments _____	Filter No. _____ Filter Type _____ Filter Tare Wt. _____ g Filter+Sample Wt. _____ g Sample Wt. _____ g
5	Test <u>Run</u> Log Number _____ Comments _____	Filter No. _____ Filter Type _____ Filter Tare Wt. _____ g Filter+Sample Wt. _____ g Sample Wt. _____ g

Results:

Field Blk. Run 1 Run 2 Run 3 Run 4 Run 5

	0.2354	0.1854	0.3511		
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Field Blk. Run 1 Run 2 Run 3 Run 4 Run 5

	0.4684	0.3273	0.4352		
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EPA Method 5 Data Reporting Sheet
Impinger Catch/Wisconsin Protocol

Team Leader L.P. Hayward Source Line 2 Press Vent
 Date Submitted 6-13-94 Test Site RTO Stack
 Test No. 14 Date of Test 6-9-94
 Date of Analysis 6-29-94 No. of Runs Completed 3
 Technician C. Helgeson

	Solvent Phase	Aqueous Phase
Test <u>14</u> Run <u>0</u> Field Blank Log Number <u>3097-1741</u> Comments _____	Dish No. <u>50</u> Dish Tare Wt. <u>48.3200</u> g Dish+Sample Wt. <u>48.3204</u> g Sample Wt. <u>0.0004</u> g	Dish No. <u>190</u> Dish Tare Wt. <u>47.5413</u> g Dish+Sample Wt. <u>47.5416</u> g Sample Wt. <u>0.0003</u> g
Test <u>14</u> Run <u>1</u> Log Number <u>-175E</u> Comments _____	Dish No. <u>53</u> Dish Tare Wt. <u>47.4067</u> g Dish+Sample Wt. <u>47.4099</u> g Sample Wt. <u>0.0032</u> g	Dish No. <u>200</u> Dish Tare Wt. <u>44.9349</u> g Dish+Sample Wt. <u>44.9493</u> g Sample Wt. <u>0.0144</u> g
Test <u>14</u> Run <u>2</u> Log Number <u>-176E</u> Comments _____	Dish No. <u>62</u> Dish Tare Wt. <u>43.1548</u> g Dish+Sample Wt. <u>43.1576</u> g Sample Wt. <u>0.0028</u> g	Dish No. <u>203</u> Dish Tare Wt. <u>46.8671</u> g Dish+Sample Wt. <u>46.8763</u> g Sample Wt. <u>0.0092</u> g
Test <u>14</u> Run <u>3</u> Log Number <u>-177E</u> Comments _____	Dish No. <u>65</u> Dish Tare Wt. <u>44.6586</u> g Dish+Sample Wt. <u>44.6616</u> g Sample Wt. <u>0.0030</u> g	Dish No. <u>209</u> Dish Tare Wt. <u>43.2082</u> g Dish+Sample Wt. <u>43.2179</u> g Sample Wt. <u>0.0097</u> g
Test _____ Run _____ Log Number _____ Comments _____	Dish No. _____ Dish Tare Wt. _____ g Dish+Sample Wt. _____ g Sample Wt. _____ g	Dish No. _____ Dish Tare Wt. _____ g Dish+Sample Wt. _____ g Sample Wt. _____ g
Test _____ Run _____ Log Number _____ Comments _____	Dish No. _____ Dish Tare Wt. _____ g Dish+Sample Wt. _____ g Sample Wt. _____ g	Dish No. _____ Dish Tare Wt. _____ g Dish+Sample Wt. _____ g Sample Wt. _____ g

Results Solvent Phases:

Field Blk.	Run 1	Run 2	Run 3	Blank Solvent Wt. <u>0.0004</u> g	Run 4	Run 5
	<u>0.0028</u>	<u>0.0024</u>	<u>0.0026</u>			

Results Aqueous Phase:

Field Blk.	Run 1	Run 2	Run 3	Run 4	Run 5
	<u>0.0141</u>	<u>0.0089</u>	<u>0.0094</u>		<u>E-21</u>

LSC-03WYR

EPA Method 5 Data Reporting Sheet
Probe/Cyclone Wash

Job L.P. Hayward Source Line 2 Press Vent
Team Leader DUH Test Site RTO Stack
Date Submitted 6-13-94 Date of Test 6-9-94
Test No. 14 No. of Runs Completed 3
Date of Analysis 6-30-94 Technician C. Helgeson
Transport Leakage ☒ None ☐ _____ ml Solvent Acetone

Test <u>14</u> Run <u>3</u> Field Blank Log Number <u>3097-174P</u> Vol. of Solvent <u>100</u> ml *Solvent Residue <u>3.0</u> ug/ml	Dish No. <u>79</u> Dish Tare Wt. <u>47.6400</u> g Dish+Sample Wt. <u>47.6403</u> g Sample Wt. _____ g
Test <u>14</u> Run <u>1</u> Vol. of Solvent <u>60</u> ml Log Number <u>-175P</u> Comments _____	Dish No. <u>80</u> Dish Tare Wt. <u>49.6254</u> g Dish+Sample Wt. <u>49.6726</u> g Sample Wt. <u>0.0472</u> g
Test <u>14</u> Run <u>2</u> Vol. of Solvent <u>60</u> ml Log Number <u>-176P</u> Comments _____	Dish No. <u>84</u> Dish Tare Wt. <u>49.1000</u> g Dish+Sample Wt. <u>49.1079</u> g Sample Wt. <u>0.0079</u> g
Test <u>14</u> Run <u>3</u> Vol. of Solvent <u>110</u> ml Log Number <u>-177P</u> Comments _____	Dish No. <u>407</u> Dish Tare Wt. <u>47.9943</u> g Dish+Sample Wt. <u>48.0157</u> g Sample Wt. <u>0.0214</u> g
Test _____ Run _____ Vol. of Solvent _____ ml Log Number _____ Comments _____	Dish No. _____ Dish Tare Wt. _____ g Dish+Sample Wt. _____ g Sample Wt. _____ g
Test _____ Run _____ Vol. of Solvent _____ ml Log Number _____ Comments _____	Dish No. _____ Dish Tare Wt. _____ g Dish+Sample Wt. _____ g Sample Wt. _____ g

*Solvent Residue _____ ug/ml = [(Sample Wt. _____ g) (10⁶)] / Vol. of Sol. _____ ml
EPA-M5 Acetone Residue Blank Spec. (7.3 ug/ml)

Results:

Field Blk. Run 1 Run 2 Run 3 Run 4 Run 5

	0.0470	0.0077	0.0211		E-22
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LSC-01YR

EPA Method 5 Data Reporting Sheet
Filter Gravimetrics

Job L.P. Hayward Source Line 2 Press Vent
Team Leader DWH Test Site RT0 Stack
Date Submitted 6-13-94 Date of Test 6-9-94
Test No. 14 No. of Runs Completed 3
Date of Analysis 6-27-94 Technician C. Helgeson

0	Test <u>14</u> Run <u>0</u> Field Blank Log Number <u>3097-174F</u> Comments _____	Filter No. <u>4010</u> Filter Type <u>4" Pallflex</u> Filter Tare Wt. <u>0.6167</u> g Filter+Sample Wt. <u>0.6170</u> g Sample Wt. <u>0.0003</u> g
1	Test <u>14</u> Run <u>1</u> Log Number <u>-175F</u> Comments _____	Filter No. <u>4007</u> Filter Type <u>4" Pallflex</u> Filter Tare Wt. <u>0.6145</u> g Filter+Sample Wt. <u>0.6191</u> g Sample Wt. <u>0.0046</u> g
2	Test <u>14</u> Run <u>2</u> Log Number <u>-176F</u> Comments _____	Filter No. <u>4008</u> Filter Type <u>4" Pallflex</u> Filter Tare Wt. <u>0.6300</u> g Filter+Sample Wt. <u>0.6344</u> g Sample Wt. <u>0.0044</u> g
3	Test <u>14</u> Run <u>3</u> Log Number <u>-177F</u> Comments _____	Filter No. <u>4009</u> Filter Type <u>4" Pallflex</u> Filter Tare Wt. <u>0.6160</u> g Filter+Sample Wt. <u>0.6177</u> g Sample Wt. <u>0.0017</u> g
4	Test _____ Run _____ Log Number _____ Comments _____	Filter No. _____ Filter Type _____ Filter Tare Wt. _____ g Filter+Sample Wt. _____ g Sample Wt. _____ g
5	Test _____ Run _____ Log Number _____ Comments _____	Filter No. _____ Filter Type _____ Filter Tare Wt. _____ g Filter+Sample Wt. _____ g Sample Wt. _____ g

Results:

Field Blk. Run 1 Run 2 Run 3 Run 4 Run 5

	0.0046	0.0044	0.0017		
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Field Blk. Run 1 Run 2 Run 3 Run 4 Run 5

	0.0685	0.0234	0.0348		
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EPA Method 5 Data Reporting Sheet
Impinger Catch/Wisconsin Protocol

Job L.P. Hayward Source Line 1 Korus
Team Leader ET Test Site Stack
Date Submitted 6-13-94 Date of Test 6-8-94
Test No. 5 No. of Runs Completed 3
Date of Analysis 6-29-94 Technician C. Helgeson

	Solvent Phase	Aqueous Phase
0	Test <u>5</u> Run <u>0</u> Field Blank Log Number <u>3097-1672</u> Comments _____ Dish No. <u>395</u> Dish Tare Wt. <u>47.2164</u> g Dish+Sample Wt. <u>47.2168</u> g Sample Wt. <u>0.0004</u> g	Dish No. <u>18</u> Dish Tare Wt. <u>49.9921</u> g Dish+Sample Wt. <u>49.9924</u> g Sample Wt. <u>0.0003</u> g
1	Test <u>5</u> Run <u>1</u> Log Number <u>-1682</u> Comments _____ Dish No. <u>405</u> Dish Tare Wt. <u>48.4908</u> g Dish+Sample Wt. <u>48.4935</u> g Sample Wt. <u>0.0027</u> g	Dish No. <u>27</u> Dish Tare Wt. <u>52.4441</u> g Dish+Sample Wt. <u>52.4514</u> g Sample Wt. <u>0.0073</u> g
2	Test <u>5</u> Run <u>2</u> Log Number <u>1692</u> Comments _____ Dish No. <u>410</u> Dish Tare Wt. <u>50.5575</u> g Dish+Sample Wt. <u>50.5606</u> g Sample Wt. <u>0.0031</u> g	Dish No. <u>32</u> Dish Tare Wt. <u>42.4904</u> g Dish+Sample Wt. <u>42.5049</u> g Sample Wt. <u>0.0145</u> g
3	Test <u>5</u> Run <u>3</u> Log Number <u>1202</u> Comments _____ Dish No. <u>501</u> Dish Tare Wt. <u>47.2525</u> g Dish+Sample Wt. <u>47.2538</u> g Sample Wt. <u>0.0013</u> g	Dish No. <u>33</u> Dish Tare Wt. <u>47.9387</u> g Dish+Sample Wt. <u>47.9472</u> g Sample Wt. <u>0.0085</u> g
4	Test _____ Run _____ Log Number _____ Comments _____ Dish No. _____ Dish Tare Wt. _____ g Dish+Sample Wt. _____ g Sample Wt. _____ g	Dish No. _____ Dish Tare Wt. _____ g Dish+Sample Wt. _____ g Sample Wt. _____ g
5	Test _____ Run _____ Log Number _____ Comments _____ Dish No. _____ Dish Tare Wt. _____ g Dish+Sample Wt. _____ g Sample Wt. _____ g	Dish No. _____ Dish Tare Wt. _____ g Dish+Sample Wt. _____ g Sample Wt. _____ g

Results Solvent Phase:

Field Blk.	Run 1	Run 2	Run 3	Blank Solvent Wt. <u>0.0004</u> g	Run 4	Run 5
	<u>0.0023</u>	<u>0.0027</u>	<u>0.0009</u>			

Results Aqueous Phase:

Field Blk.	Run 1	Run 2	Run 3	Run 4	Run 5
	<u>0.0070</u>	<u>0.0142</u>	<u>0.0082</u>		<u>E-24</u>

LSC-03WYR

EPA Method 5 Data Reporting Sheet
Probe/Cyclone Wash

Job L.P. Hayward Source Line 1 Konus
Team Leader CT Test Site Stack
Date Submitted 6-13-94 Date of Test 6-8-94
Test No. 5 No. of Runs Completed 3
Date of Analysis 6-30-94 Technician C. Halgeson
Transport Leakage ☒ None ☐ ml Solvent Acetone

0	Test <u>5</u> Run <u>0</u> Field Blank Log Number <u>3097-167P</u> Vol. of Solvent <u>100</u> ml *Solvent Residue <u>3.0</u> ug/ml	Dish No. <u>64</u> Dish Tare Wt. <u>43.1473</u> g Dish+Sample Wt. <u>43.1476</u> g Sample Wt. <u>0.0003</u> g
1	Test <u>5</u> Run <u>1</u> Vol. of Solvent <u>160</u> ml Log Number <u>168P</u> Comments <u> </u>	Dish No. <u>513</u> Dish Tare Wt. <u>47.4130</u> g Dish+Sample Wt. <u>47.4450</u> g Sample Wt. <u>0.0320</u> g
2	Test <u>5</u> Run <u>2</u> Vol. of Solvent <u>160</u> ml Log Number <u>169P</u> Comments <u> </u>	Dish No. <u>522</u> Dish Tare Wt. <u>47.0006</u> g Dish+Sample Wt. <u>47.0145</u> g Sample Wt. <u>0.0139</u> g
3	Test <u>5</u> Run <u>3</u> Vol. of Solvent <u>160</u> ml Log Number <u>170P</u> Comments <u> </u>	Dish No. <u>616</u> Dish Tare Wt. <u>50.9231</u> g Dish+Sample Wt. <u>50.9400</u> g Sample Wt. <u>0.0169</u> g
4	Test <u> </u> Run <u> </u> Vol. of Solvent <u> </u> ml Log Number <u> </u> Comments <u> </u>	Dish No. <u> </u> Dish Tare Wt. <u> </u> g Dish+Sample Wt. <u> </u> g Sample Wt. <u> </u> g
5	Test <u> </u> Run <u> </u> Vol. of Solvent <u> </u> ml Log Number <u> </u> Comments <u> </u>	Dish No. <u> </u> Dish Tare Wt. <u> </u> g Dish+Sample Wt. <u> </u> g Sample Wt. <u> </u> g

*Solvent Residue 3.0 ug/ml = ((Sample Wt. 0.0003g) (100)) / Vol. of Sol. 100 ml
EPA-M5 Acetone Residue Blank Spec. {7.3 ug/ml

Results:

Field Blk. Run 1 Run 2 Run 3 Run 4 Run 5

	<u>0.0315</u>	<u>0.0134</u>	<u>0.0164</u>		<u>E-25</u>
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LSC-01YR

EPA Method 5 Data Reporting Sheet
Filter Gravimetrics

Job L.P. Hayward Source Line 1 Konus
Team Leader ET Test Site Stack
Date Submitted 6-13-94 Date of Test 4" Pallflex
Test No. 5 No. of Runs Completed 3
Date of Analysis 6-27-94 Technician C. Helgeson

0	Test <u>5</u> Run <u>0</u> Field Blank Log Number <u>3097-167F</u> Comments _____	Filter No. <u>4034</u> Filter Type <u>4" Pallflex</u> Filter Tare Wt. <u>0.6240</u> g Filter+Sample Wt. <u>0.6242</u> g Sample Wt. <u>0.0002</u> g
1	Test <u>5</u> Run <u>1</u> Log Number <u>-168F</u> Comments _____	Filter No. <u>4031</u> Filter Type <u>4" Pallflex</u> Filter Tare Wt. <u>0.6230</u> g Filter+Sample Wt. <u>0.6565</u> g Sample Wt. <u>0.0335</u> g
2	Test <u>5</u> Run <u>2</u> Log Number <u>-169F</u> Comments _____	Filter No. <u>4032</u> Filter Type <u>4" Pallflex</u> Filter Tare Wt. <u>0.6240</u> g Filter+Sample Wt. <u>0.6360</u> g Sample Wt. <u>0.0120</u> g
3	Test <u>5</u> Run <u>3</u> Log Number <u>-170F</u> Comments _____	Filter No. <u>4033</u> Filter Type <u>4" Pallflex</u> Filter Tare Wt. <u>0.6302</u> g Filter+Sample Wt. <u>0.6560</u> g Sample Wt. <u>0.0258</u> g
4	Test _____ Run _____ Log Number _____ Comments _____	Filter No. _____ Filter Type _____ Filter Tare Wt. _____ g Filter+Sample Wt. _____ g Sample Wt. _____ g
5	Test _____ Run _____ Log Number _____ Comments _____	Filter No. _____ Filter Type _____ Filter Tare Wt. _____ g Filter+Sample Wt. _____ g Sample Wt. _____ g

Results:

Field Blk. Run 1 Run 2 Run 3 Run 4 Run 5

	0.0335	0.0120	0.0258		
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Field Blk. Run 1 Run 2 Run 3 Run 4 Run 5

	0.0743	0.0423	0.0513		
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EPA Method 5 Data Reporting Sheet
Impinger Catch/Wisconsin Protocol

Job L.P. Hayward Source Line 2 Kouns
Team Leader MK Test Site Stack
Date Submitted 6-13-94 Date of Test 6-8-94
Test No. 16 No. of Runs Completed 3
Date of Analysis 6-29-94 Technician C. Helgeson

	Solvent Phase	Aqueous Phase
0	Test <u>Run 0</u> Field Blank Log Number Comments	Dish No. _____ Dish Tare Wt. _____ g Dish+Sample Wt. _____ g Sample Wt. _____ g
1	Test <u>16</u> Run <u>1</u> Log Number <u>3097-178F</u> Comments	Dish No. <u>51</u> Dish Tare Wt. <u>48.8515</u> g Dish+Sample Wt. <u>48.8560</u> g Sample Wt. <u>0.0045</u> g
2	Test <u>16</u> Run <u>2</u> Log Number <u>179I</u> Comments	Dish No. <u>54</u> Dish Tare Wt. <u>49.6696</u> g Dish+Sample Wt. <u>49.6725</u> g Sample Wt. <u>0.0029</u> g
3	Test <u>16</u> Run <u>3</u> Log Number <u>180I</u> Comments	Dish No. <u>56</u> Dish Tare Wt. <u>47.7598</u> g Dish+Sample Wt. <u>47.7596</u> g Sample Wt. <u>0.0038</u> g
4	Test <u>Run</u> Log Number Comments	Dish No. _____ Dish Tare Wt. _____ g Dish+Sample Wt. _____ g Sample Wt. _____ g
5	Test <u>Run</u> Log Number Comments	Dish No. _____ Dish Tare Wt. _____ g Dish+Sample Wt. _____ g Sample Wt. _____ g

Results Solvent Phase:

Field Blk.	Run 1	Run 2	Run 3	Blank Solvent Wt. <u>0.0004</u> g	Run 4	Run 5
	<u>0.0041</u>	<u>0.0025</u>	<u>0.0034</u>			

Results Aqueous Phase:

Field Blk.	Run 1	Run 2	Run 3	Run 4	Run 5
	<u>0.0140</u>	<u>0.0142</u>	<u>0.0085</u>		<u>E-27</u>

LSC-03WYR

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(612) 786-6020

EPA Method 5 Data Reporting Sheet
Probe/Cyclone Wash

Job L.P. Hayward Source Line 2 Ronus
Team Leader MK Test Site Stack
Date Submitted 6-13-94 Date of Test 6-8-94
Test No. 16 No. of Runs Completed 3
Date of Analysis 6-30-94 Technician C. Helgeson
Transport Leakage ☒ None ml Solvent Acetone

3	Test <u>Run 0</u> Field Blank Log Number _____ Vol. of Solvent _____ ml *Solvent Residue <u>3.0</u> ug/ml	Dish No. _____ Dish Tare Wt. _____ g Dish+Sample Wt. _____ g Sample Wt. _____ g
1	Test <u>16</u> Run <u>1</u> Vol. of Solvent <u>170</u> ml Log Number <u>3097-178P</u> Comments _____	Dish No. <u>19</u> Dish Tare Wt. <u>48.9566</u> g Dish+Sample Wt. <u>48.9692</u> g Sample Wt. <u>0.0126</u> g
2	Test <u>16</u> Run <u>2</u> Vol. of Solvent <u>190</u> ml Log Number <u>179P</u> Comments _____	Dish No. <u>21</u> Dish Tare Wt. <u>47.5275</u> g Dish+Sample Wt. <u>47.5468</u> g Sample Wt. <u>0.0193</u> g
3	Test <u>16</u> Run <u>3</u> Vol. of Solvent <u>160</u> ml Log Number <u>180P</u> Comments _____	Dish No. <u>28</u> Dish Tare Wt. <u>46.0409</u> g Dish+Sample Wt. <u>46.0570</u> g Sample Wt. <u>0.0161</u> g
4	Test _____ Run _____ Vol. of Solvent _____ ml Log Number _____ Comments _____	Dish No. _____ Dish Tare Wt. _____ g Dish+Sample Wt. _____ g Sample Wt. _____ g
5	Test _____ Run _____ Vol. of Solvent _____ ml Log Number _____ Comments _____	Dish No. _____ Dish Tare Wt. _____ g Dish+Sample Wt. _____ g Sample Wt. _____ g

*Solvent Residue ug/ml = [(Sample Wt. g) (10⁶)] / Vol. of Sol. ml
EPA-MS Acetone Residue Blank Spec. (7.3 ug/ml)

Results:

Field Blk. Run 1 Run 2 Run 3 Run 4 Run 5

	0.0121	0.0187	0.0156		E-28
--	--------	--------	--------	--	------

LSC-01YR

EPA Method 5 Data Reporting Sheet
Filter Gravimetrics

Job L.P. Hayward Source Line 2 Korus
Team Leader MK Test Site Spack
Date Submitted 6-13-94 Date of Test 6-8-94
Test No. 16 No. of Runs Completed 3
Date of Analysis 6-27-94 Technician C. Helgeson

0	Test <u>Run 0</u> Field Blank Log Number _____ Comments _____	Filter No. _____ Filter Type _____ Filter Tare Wt. _____ g Filter+Sample Wt. _____ g Sample Wt. _____ g
1	Test <u>16 Run 1</u> Log Number <u>3097-178F</u> Comments _____	Filter No. <u>4035</u> Filter Type <u>4" Pallflex</u> Filter Tare Wt. <u>0.6176</u> g Filter+Sample Wt. <u>0.6638</u> g Sample Wt. <u>0.0462</u> g
2	Test <u>16 Run 2</u> Log Number <u>179F</u> Comments _____	Filter No. <u>4036</u> Filter Type <u>4" Pallflex</u> Filter Tare Wt. <u>0.6282</u> g Filter+Sample Wt. <u>0.6448</u> g Sample Wt. <u>0.0166</u> g
3	Test <u>16 Run 3</u> Log Number <u>-180F</u> Comments _____	Filter No. <u>4037</u> Filter Type <u>4" Pallflex</u> Filter Tare Wt. <u>0.6276</u> g Filter+Sample Wt. <u>0.6455</u> g Sample Wt. <u>0.0179</u> g
4	Test <u>Run</u> Log Number _____ Comments _____	Filter No. _____ Filter Type _____ Filter Tare Wt. _____ g Filter+Sample Wt. _____ g Sample Wt. _____ g
5	Test <u>Run</u> Log Number _____ Comments _____	Filter No. _____ Filter Type _____ Filter Tare Wt. _____ g Filter+Sample Wt. _____ g Sample Wt. _____ g

Results:

Field Blk. Run 1 Run 2 Run 3 Run 4 Run 5

	0.0462	0.0166	0.0179		
--	--------	--------	--------	--	--

Field Blk. Run 1 Run 2 Run 3 Run 4 Run 5

	0.0764	0.0520	0.0454		
--	--------	--------	--------	--	--

Interpoli Laboratories
(612)786-6020

EPA Method 7A Recovery and Analysis Data Sheet (1)

*****SOURCE*****
Job L.P. Hayward
Source Line 1 Kowals
Date of Sampling 6-8-94
Test No(s) 5

*****RECOVERY*****
Date of Recovery 6-16-94
Recovered by C.G.
Recovery volume 500ml ml
Barometric at time 28.97 IN.HG.

*****ANALYTICAL*****
Date of Analysis 6-22-94
Analyst ADH
Eluent ADH
Chromatograph: Dionex System 4000i

Samples collected in accordance with EPA Method 7, CFR Title 40, Part 60, Appendix A. Samples analyzed in accordance with EPA Method 7A by ion chromatography. Mercury manometers used to measure flask pressures/vacuums in sampling and in recovery. Thommen Model TX 19 jewel barometer calibrated against laboratory mercury in glass barometer used to measure field barometric pressure. Three field blanks are prepared and the average used to correct measured nitrate concentrations. All samples are analyzed as a batch using a Dionex Model 4270 Chromatograph Data Integrator. The integrator is programmed to give the actual concentration of the 500 ml recovered sample even if a subsequent dilution was made. The dilution is indicated here as well as on the chromatogram.

$$C_{RS} = DF(C_{DS}) \quad M_{NO_3} = (C_{RS} - \bar{C}_B)V_R \quad \bar{C}_B = (C_{B1} + C_{B2} + C_{B3})/3$$

where:

C_{RS} = concentration of nitrate in 500 ml recovered sample in ug/ml

DF = dilution factor

C_{DS} = concentration of nitrate of a 500 ml recovered sample which has been diluted by a factor of DF to bring it into the proper range for the ion chromatograph. This value is an intermediate number and is not outputted by the electronic integrator which is programmed to output the concentration of the original undiluted 500 ml recovered sample.

M_{NO_3} = total mass of nitrate in micrograms in the 500 ml recovered sample and/or in the 2L flask.

C_B = average conc. of nitrate in 500 ml recovered samples from the three field blanks (ug/ml)

C_{B1}, C_{B2}, C_{B3} = conc. of nitrate in 500 ml recovered samples from the three field blanks (ug/ml)

V_R = recovery volume for samples and field blanks in ml

EPA Method 7A Recovery and Analysis Data Sheet (2)

1

S-340(2) R-9/85

Interpoll Laboratories
(612)786-6020

EPA Method 7A Recovery and Analysis Data Sheet (1)

*****SOURCE*****
Job L.P. Hayward
Source Line 2
Date of Sampling 6-8-94
Test No(s) 16

*****RECOVERY*****
Date of Recovery 6-16-94
Recovered by C.G.
Recovery volume 500ml ml
Barometric at time 28.97 IN.HG.

*****ANALYTICAL*****
Date of Analysis 6-22-94
Analyst AKH
Eluent ACN
Chromatograph: Dionex System 4000i

Samples collected in accordance with EPA Method 7, CFR Title 40, Part 60, Appendix A. Samples analyzed in accordance with EPA Method 7A by ion chromatography. Mercury manometers used to measure flask pressures/vacuums in sampling and in recovery. Thommen Model TX 19 jewel barometer calibrated against laboratory mercury in glass barometer used to measure field barometric pressure. Three field blanks are prepared and the average used to correct measured nitrate concentrations. All samples are analyzed as a batch using a Dionex Model 4270 Chromatograph Data Integrator. The integrator is programmed to give the actual concentration of the 500 ml recovered sample even if a subsequent dilution was made. The dilution is indicated here as well as on the chromatogram.

$$C_{RS} = DF(C_{DS}) \quad M_{NO_3} = (C_{RS} - \bar{C}_B)V_R \quad \bar{C}_B = (C_{B1} + C_{B2} + C_{B3})/3$$

where:

C_{RS} = concentration of nitrate in 500 ml recovered sample in ug/ml

DF = dilution factor

C_{DS} = concentration of nitrate of a 500 ml recovered sample which has been diluted by a factor of DF to bring it into the proper range for the ion chromatograph. This value is an intermediate number and is not outputted by the electronic integrator which is programmed to output the concentration of the original undiluted 500 ml recovered sample.

M_{NO_3} = total mass of nitrate in micrograms in the 500 ml recovered sample and/or in the 2L flask.

$\bar{C}_B$ = average conc. of nitrate in 500 ml recovered samples from the three field blanks (ug/ml)

C_{B1}, C_{B2}, C_{B3} = conc. of nitrate in 500 ml recovered samples from the three field blanks (ug/ml)

V_R = recovery volume for samples and field blanks in ml

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S-305RR
(9/90)

EPA Method 10 NDIR Analysis

Job Name L.P. Hayward
Source Press RTO outlet Stack (6-7-94)
Date of Analysis 6-15-94
Technician C. Hefeson

NDIR Analyzer: ☐ Fugl ACS Model 3300
☐ Mon. Lab Model 8310
☒ Dasibi Model 3003
Range: 0 - 200 ppm
Flow rate: 600 cc/min

Pretest Calibration				Post-test Calibration			
Sample Description Test/Run	Conc.	Reading	Vendor	Cyl. Number	Conc.	Reading	Vendor
Zero gas:	0	ppm	0	ppm	0	ppm	Scott
Upscale gas:	41.5	ppm	41.5	ppm	41.5	ppm	National
Upscale gas:	204	ppm	41.5	ppm	204	ppm	National
Upscale gas:		ppm		ppm		ppm	

Sample Description Test/Run	Sample Log Number	CO Conc. (ppm, Dry)		
		Dilution Factor	Reading	Actual ppm
3/1	3047-113	-	11.3	11.3
3/2	-114	-	12.9	12.9
3/3	-115	-	12.5	12.5

Sample Description Test/Run	Sample Log Number	CO Conc. (ppm, Dry)		
		Dilution Factor	Reading	Actual ppm

Note 1: If sample dilution is required the sample is diluted with CO-free gas prior to analysis.

Note 2: The Fugl ACS model 3300 has a rejection ratio for CO to CO₂ greater than 100,000; 1 and the Mon. Labs Model 8310 and Dasibi Model 3003 have rejection ratios greater than 200,000; 1 and thus CO₂ removal prior to analysis is not required.

Note 3: The analyzer must be zeroed and spanned immediately before and after sample analysis. Additional checks may be performed between sample analyses if required.

EPA Method 7A Recovery and Analysis Data Sheet (2)

[illegible]

1

S-340(2) R-9/85

EPA Method 10 NDIR Analyze 18

Job Name L.P. Hayward
Source Line 1 Kanus Stack
Date of Analysis 6-15-94
Technician C. Halgeson

Pretest Calibration				Post-test Calibration			
Conc.	Reading	Vendor	Cyl. Number	Conc.	Reading	Vendor	Cyl. Number
Zero gas: 0 ppm	0 ppm	Scott	AAL 17431	Zero gas: 0 ppm	0 ppm	Scott	AAL 17431
Upscale gas: 41.5 ppm	41.5 ppm	National	CC 52502	Upscale gas: 41.5 ppm	41.5 ppm	National	CC 52502
Upscale gas: 204 ppm	204 ppm	National	CC 81624	Upscale gas: 204 ppm	204 ppm	National	CC 81624
Upscale gas: _____ ppm	_____ ppm	_____	_____	Upscale gas: _____ ppm	_____ ppm	_____	_____

[illegible][illegible]

Note 1: If sample dilution is required the sample is diluted with CO-free gas prior to analysis.

Note 2: The Fugl ACS model 3300 has a rejection ratio for CO to CO₂ greater than 100,000; 1 and the Mon. Labs Model 8310 and Dasibi Model 3003 have rejection ratios greater than 200,000; 1 and thus CO₂ removal prior to analysis is not required.

Note 3: The analyzer must be zeroed and spanned immediately before and after sample analysis. Additional checks may be performed between sample analyses if required.

```

NDIR Analyzer: ☐ Fug: ACS Model 3300
                ☐ Mon. Lab Model 8310
                ☒ Dasibi Model 3003
                Range: 0 - 200 ppm
                Flow rate: 1000 cc/min

```

Post-test Calibration

Conc.	Reading	Vendor	Cyl. Number
Zero gas:	0 ppm	Scott	AAL 17431
Upscale gas:	41.5 ppm	National	CC 52502
Upscale gas:	104 ppm	National	CC 81624
Upscale gas:	ppm		

[illegible]

Note 3: The analyzer must be zeroed and spanned immediately before and after sample analysis. Additional checks may be performed between sample analyses if required.

INTERPOLL LABORATORIES INC.

Formaldehyde Results Using EPA Method 0011
For Dept. 20/LP Hayward Wi. Collected 6/7-10/94

	Field Spike #1			Test: 1		Source: RTO Press Outlet Stack	
	Actual	Found	% Recovery	Run 0	Run 1	Run 2	Run 3
Log #		(3097-05)		(3097-01)	(3097-02)	(3097-03)	(3097-04)
Mass (ug)*	750	451	60.1	2.6	430	14	610

	Field Spike #2			Test: 6		Source: Line 1 Konus Stack	
	Actual	Found	% Recovery	Run 0	Run 1	Run 2	Run 3
Log #		(3097-06)			(3097-07)	(3097-08)	(3097-09)
Mass (ug)*	750	521	69.5		56	140	79

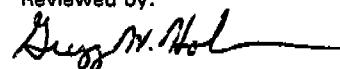
	Field Spike #3			Test: 12		Source: Line 2 RTO Press Vent Stack	
	Actual	Found	% Recovery	Run 0	Run 1	Run 2	Run 3
Log #		(3097-16)		(3097-18)	(3097-19/20)	(3097-21/22)	(3097-23/24)
Mass (ug)*	750	575	76.7	1.6	400	340	360

	Field Spike #5			Test: 17		Source: Line 2 Konus Stack	
	Actual	Found	% Recovery	Run 0	Run 1	Run 2	Run 3
Log #		(3097-10)			(3097-11)	(3097-12)	(3097-13)
Mass (ug)*	750	513	68.4		94	66	140

	Field Spike #4			Field Spike #6		
	Actual	Found	% Recovery	Actual	Found	% Recovery
Log #		(3097-15)			(3097-17)	
Mass (ug)*	750	567	75.6	750	575	76.7

* = Total Mass of formaldehyde in the sample in ug. The laboratory method blanks contained 1.1ug and 0.66ug.

Reviewed by:


Gregg W. Holman

INTERPOLL LABORATORIES INC.

4,4-Methylenebis(phenyl isocyanate) Results
For Dept. 20/LP Hayward Collected 6/8-9/94

Item	Field Spike			Test: 2	Source: Press RTO Outlet Stack		
	Actual	Found	% Rec.	Run 0	Run 1	Run 2	Run 3
EPA Draft Method 1,2-PP Impinger 1							
Log #		3097-31		NP	3097-25	3097-27	3097-29
Date Analyzed		7/5/94		NP	7/5/94	7/5/94	7/5/94
Mass (ug)*	296	256	86	NP	< 2.5	< 2.5	< 2.5
EPA Draft Method 1,2-PP Impinger 2							
Log #				NP	3097-26	3097-28	3097-30
Date Analyzed				NP	7/5/94	7/5/94	7/5/94
Mass (ug)*				NP	5.2	< 2.5	5.4

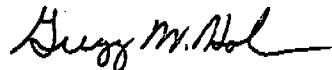
Item	Field Spike			Test: 13	Source: Line 2 Press Vent RTO Stack		
	Actual	Found	% Rec.	Run 0	Run 1	Run 2	Run 3
EPA Draft Method 1,2-PP Impinger 1							
Log #		NR		3097-32	3097-33	3097-35	3097-37
Date Analyzed		NR		7/5/94	7/5/94	7/5/94	7/5/94
Mass (ug)*	NR	NR	NR	< 2.5	12.2	< 2.5	< 2.5
EPA Draft Method 1,2-PP Impinger 2							
Log #				NR	3097-34	3097-36	3097-38
Date Analyzed				NR	7/5/94	7/5/94	7/5/94
Mass (ug)*				NR	< 2.5	< 2.5	6.5

NP = Not Provided

NR = Not Required

* = Total Mass of MDI in the Sample in ug.

Reviewed By:


Gregg W. Holman

Client: I.D. 020 C.P. Hayward

Sample Collected: _____

Sample Received: _____

Sample Log #: 3097-95

Sample Description: charcoal tube

Line 2: Konus Stack
Test 20 Run 1
1 of 2

			FRONT			BACK		
Parameter	Units	Analysis Date & Initials	Detection Limit Front	Analytical Result Front	Method Blank Front	Detection Limit Back	Analytical Result Back	Method Blank Back
Benzene	Total ug	MMA N	< 0.1	< 2.1	< 2.1	x .61	< .61	< .61
Toluene	Total ug	W-29H						
Ethylbenzene	Total ug							
Xylenes	Total ug							
Dilution factor								
Total hydrocarbons as gasoline	Total ug							
Dilution factor								

notes:

In-House Comments: channel was wet

Client: I.D. 020 C.P. Hayward

Sample Collected: _____

Sample Received: _____

T 20 R 1

2 of 2

Sample Log #: 3097-96

Sample Description: charcoal tube

			FRONT			BACK		
Parameter	Units	Analysis Date & Initials	Detection Limit Front	Analytical Result Front	Method Blank Front	Detection Limit Back	Analytical Result Back	Method Blank Back
Benzene	Total ug	MMH	< 2.1	< 2.1	< 2.1	< .61	< .61	< .61
Toluene	Total ug	10/20/94						
Ethylbenzene	Total ug							
Xylenes	Total ug							
Dilution factor								
Total hydrocarbons as gasoline	Total ug							
Dilution factor								

Footnotes: _____

In-House Comments: Channel was wet

LCI-127

Client: I.D. 020 C.P. Hayward

Sample Received: _____

Sample Log #: 3097-97

Sample Description: charcoal tube

T20 R2
1 of 2

Footnotes: _____

In-House Comments: _____

Client: I.D. 020 C.P. Hayward

Sample Received: _____

Sample Log #: 3097-98

Sample Description: charcoal tube

T 20 R 2
2 of 2

Parameter	Units	Analysis Date & Initials	FRONT			BACK		
			Detection Limit Front	Analytical Result Front	Method Blank Front	Detection Limit Back	Analytical Result Back	Method Blank Back
Benzene	Total ug	<i>MM</i>	<i>x 2.1</i>	<i>< 2.1</i>	<i>< 2.1</i>	<i>x .61</i>	<i>< .61</i>	<i>< .61</i>
Toluene	Total ug	<i>6-2294</i>						
Ethylbenzene	Total ug							
Xylenes	Total ug							
Dilution factor								
Total hydrocarbons as gasoline	Total ug							
Dilution factor								

Footnotes: _____

In-House Comments: _____

LCI-127

Client: I.D. 020 C.P. Hayward

Sample Collected: _____

Sample Received: _____

T 20 R 3

1 of 2

Sample Log #: 3097-99

Sample Description: charcoal tube

			FRONT			BACK		
Parameter	Units	Analysis Date & Initials	Detection Limit Front	Analytical Result Front	Method Blank Front	Detection Limit Back	Analytical Result Back	Method Blank Back
Benzene	Total ug	MMH.	x 2.1	<2.1	<2.1	x .61	<.61	<.61
Toluene	Total ug	6-2094						
Ethylbenzene	Total ug							
lenes	Total ug							
Dilution factor								
Total hydrocarbons as gasoline	Total ug							
Dilution factor								

Notes:

In-House Comments: _____

Client: I.D. 020 C.P. Hayward

Sample Received: _____

Sample Log #: 3097-100

Sample Description: charcoal tube

T20 R3
2 of 2

Parameter	Units	Analysis Date & Initials	FRONT			BACK		
			Detection Limit Front	Analytical Result Front	Method Blank Front	Detection Limit Back	Analytical Result Back	Method Blank Back
Benzene	Total ug	<i>[Signature]</i>	x 2.1	<2.1	<2.1	x .61	<.61	<.61
Toluene	Total ug	10/22/94						
Ethylbenzene	Total ug							
Xylenes	Total ug							
Dilution factor								
Total hydrocarbons as gasoline	Total ug							
Dilution factor								

Footnotes: _____

In-House Comments: _____

LCI-127

Client: I.D. 020 C.P. Hayward

Sample Collected: 6-7

Sample Received: 6-13

Line 1 Konus Stack
Test 9 Run 1
1 of 2

Sample Log #: 3097-83

Sample Description: charcoal tube

Footnotes:

In-House Comments:

Client: I.D. 020 C.P. Hayward

Sample Collected: _____

Sample Received: _____

T9 R1

2 of 2

Sample Log #: 3097-84

Sample Description: charcoal tube

Parameter	Units	Analysis Date & Initials	FRONT			BACK		
			Detection Limit Front	Analytical Result Front	Method Blank Front	Detection Limit Back	Analytical Result Back	Method Blank Back
Benzene	Total ug	MNH	< 2.1	< 2.1	< 2.1	x .61	< .61	< .61
Toluene	Total ug	6-7-94						
Ethylbenzene	Total ug							
Xylenes	Total ug							
Dilution factor								
Total hydrocarbons as gasoline	Total ug							
Dilution factor								

Footnotes: _____

In-House Comments: _____

Client: I.D. 020 C.P. Hayward

Sample Received: _____

Sample Log #: 3097-57

Sample Description: charcoal tube

T9 R2
1 of 2

		Analysis	FRONT			BACK		
Parameter	Units	Date & Initials	Detection Limit Front	Analytical Result Front	Method Blank Front	Detection Limit Back	Analytical Result Back	Method Blank Back
Benzene	Total ug	MMM	< 2.1	< 2.1	< 2.1	< .61	< .61	< .61
Toluene	Total ug	10-21-94						
Ethylbenzene	Total ug							
Xylenes	Total ug							
Dilution factor								
Total hydrocarbons as gasoline	Total ug							
Dilution factor								

Footnotes:

In-House Comments:

Client: I.D. 020 C.P. Hayward

Sample Received: _____

T9 R2

2 of 2

Sample Log #: 3097-88

Sample Description: charcoal tube

Parameter	Units	Analysis Date & Initials	FRONT			BACK		
			Detection Limit Front	Analytical Result Front	Method Blank Front	Detection Limit Back	Analytical Result Back	Method Blank Back
Benzene	Total ug	mmx	< 2.1	< 2.1	< 2.1	< 1.61	< 1.61	< 1.61
Toluene	Total ug	10-294						
Ethylbenzene	Total ug							
Xylenes	Total ug							
Dilution factor								
Total hydrocarbons as gasoline	Total ug							
Dilution factor								

Footnotes: _____

In-House Comments: _____

Client: I.D. 020 C.P. Hayward

Sample Received: _____

T9 R3

1 of 2

Sample Log #: 3097-91

Sample Description: charcoal tube

		Analysis	FRONT			BACK		
Parameter	Units	Date & Initials	Detection Limit Front	Analytical Result Front	Method Blank Front	Detection Limit Back	Analytical Result Back	Method Blank Back
Benzene	Total ug	MMA	<2.1	<2.1	<2.1	<.601	<.601	<.601
Toluene	Total ug	LOA-94						
Ethylbenzene	Total ug							
Xylenes	Total ug							
Dilution factor								
Total hydrocarbons as gasoline	Total ug							
Dilution factor								

Notes: _____

In-House Comments:

Client: I.D. 020 C.P. Hayward

Sample Collected: _____

Sample Received: _____

Sample Log #: 3097-92

Sample Description: charcoal tube

T9R3

2 of 2

[illegible]

Footnotes: _____

In-House Comments:

LCI-127

INTERPOLL LABORATORIES INC.

Phenol Result By EPA Method 8270
For Dept. 20/ LP Hayward
Collected 6/8-9/94

	Test: 7		Source: Line 1 Konus Stack
	Run 1	Run 2	Run 3
Log #	3097-39/40	3097-41/42	3097-43/44
Analysis Date	6/20/94	6/20/94	6/20/94
Phenol*	< 840	< 840	< 840
2-Fluorophenol**	28.3	31.4	23.4
D6-Phenol**	21.4	22.1	28.1
2,4,6-Tribromophenol***	81.4	66.8	84.8

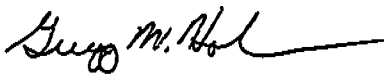
	Test: 18		Source: Line 2 Konus Stack
	Run 1	Run 2	Run 3
Log #	3097-45/46	3097-47/48	3097-49/50
Analysis Date	6/20/94	6/20/94	6/20/94
Phenol*	< 840	< 840	< 840
2-Fluorophenol**	35.8	40.8	48.7
D6-Phenol**	22.1	26.6	27.0
2,4,6-Tribromophenol***	78.5	73.1	87.3

* = Total mass of the specified compound in the sample in ug.

** = Percent recovery of the field surrogate. (59800 ug 2-Fluorophenol and 5330 ug Phenol-D6 was added to the impinger solution before sampling.)

*** = Percent recovery of the lab surrogates.

Reviewed By:


Gregg W. Holman

INTERPOLL LABORATORIES INC.

Polycyclic Organic Matter Results By EPA Method 8270
For Dept. 20/ LP Hayward, Collected 6/9/94

	Test : 8				Source: Line 1 Konus Stack			
	Run 0	Run 1	Run 2	Run 3	Run 0	Run 1	Run 2	Run 3
Log #	3097-51	3097-55	3097-59	3097-63				
Compounds of Interest								
Benz(a)anthracene*	< 1.8	< 1.8	9.4	11				
Benzo(b)fluoranthene*	< 0.99	51	26	34				
Benzo(a)pyrene*	< 1.2	13	< 1.2	9.6				
Dibenz(a,h)acridine*	< 15	< 15	< 15	< 15				
Dibenz(a,j)acridine*	< 1.6	< 1.6	< 1.6	< 1.6				
Dibenz(a,h)anthracene*	< 0.88	< 0.88	< 0.88	< 0.88				
7H-Dibenzo(c,g)carbazole*	< 1.2	< 1.2	< 1.2	< 1.2				
Dibenzo(a,h)pyrene*	< 20	< 20	< 20	< 20				
Dibenzo(a,i)pyrene*	< 20	< 20	< 20	< 20				
Indeno(1,2,3-cd)pyrene*	< 0.90	6.9	2.3	3.8				
Field Surrogate Recovery								
D10-Fluoranthene**	78.0	95.5	90.5	101				
Lab Surrogate Recovery								
D5-Nitrobenzene***	73.8	93.8	82.8	80.8				
2-Fluorobiphenyl***	70.4	96.8	88.6	88.6				
D14-Terphenyl***	92.6	101	96.2	91.2				

	Test : 19				Source: Line 2 Konus Stack			
	Run 0	Run 1	Run 2	Run 3	Run 0	Run 1	Run 2	Run 3
Log #	3097-67	3097-71	3097-75	3097-79				
Compounds of Interest								
Benz(a)anthracene*	< 1.8	< 1.8	< 1.8	< 1.8				
Benzo(b)fluoranthene*	< 0.99	< 0.99	< 0.99	< 0.99				
Benzo(a)pyrene*	2.2	4.9	< 1.2	< 1.2				
Dibenz(a,h)acridine*	< 15	< 15	< 15	< 15				
Dibenz(a,j)acridine*	< 1.6	< 1.6	< 1.6	< 1.6				
Dibenz(a,h)anthracene*	< 0.88	< 0.88	< 0.88	< 0.88				
7H-Dibenzo(c,g)carbazole*	< 1.2	< 1.2	< 1.2	< 1.2				
Dibenzo(a,h)pyrene*	< 20	< 20	< 20	< 20				
Dibenzo(a,i)pyrene*	< 20	< 20	< 20	< 20				
Indeno(1,2,3-cd)pyrene*	< 0.90	< 0.90	< 0.90	< 0.90				
Field Surrogate Recovery								
D10-Fluoranthene**	45.5	99.5	86.5	94.0				
Lab Surrogate Recovery								
D5-Nitrobenzene***	28.4	84.8	88.0	84.6				
2-Fluorobiphenyl***	36.8	88.6	94.8	84.4				
D14-Terphenyl***	58.8	95.0	107.2	95.4				

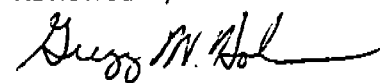
- * = Total mass of the specified compound in the sample in ug.
- ** = Percent recovery of the field surrogate.
- *** = Percent recovery of the lab surrogates.

3097SV.LPH

Page 1 of 1

E-52

Reviewed By:


Gregg W. Holman
Laboratory Director

Interpoll Laboratories
(612) 786-6020

IMPINGER CATCHES

Project Name: LP/Hayward Order Date: _____
Date Required: 6/6/94 Delivery Date: 6/3/94

Nature of Spiking Material	Spike Concentration	Spike Volume	Total Mass of Spike
D-6 Phenol (P-67)	5.3316 mg/mL	1.0 mL	5.3316 mg
2-fluorophenol (P-68)	49.8140 mg/mL	1.2 mL	59.7768 mg

SPECIAL REQUIREMENTS

WAD 6/1/94

**Please return this form with the samples.

INTERPOL LABORATORIES, INC.

(612) 786-6020

Sample Chain of Custody

Job
Field Engineer

Log No.
No. of Runs

Source
Date of Test

Site
Test No.

LP-HAYWARD
5-23

REBS 2010 SUPER
6-7-94

STACK
1

3097
3

No. Items	Sample Type	Analysis	Sequence No.	Comments
4	Probe Wash: ☐ Acetone ☒ MeCl ₂	☐ DI Water ☐ _____		
0	Filter: ☐ 4" Glass ☐ 55 Thimble	☐ Pallflex ☐ 2.5" Glass		
4	Impingers: ☐ DI Water ☐ 3% H ₂ O ₂ ☐ 1N NaOH ☒ 4 DNPH	☐ H ₂ SO ₄ ☐ HNO ₃ /H ₂ O ₂ ☐ KMnO ₄ /H ₂ SO ₄ ☐ _____		
3	Integrated Gas: ☐ Tedlar Bag	☐ EPA M-3 ☐ _____		
0	Oxides of Nitrogen:	☐ EPA M-7A ☐ _____		
0	Fuel Lab: ☐ Fuel Sample	☐ Per S-0163		
0	Particle Sizing:	☐ X-Ray Scatograph ☐ Cascade Imp		
1	Miscellaneous:	☒ Fuel Spill		

Misc: ☒ Natural Gas
☐ RDF
☐ _____

Oil: ☐ Waste Oil
☐ No. 2
☐ No. 6

Wood: ☐ Wood Waste
☐ Dust
☐ Bark

Coal: ☐ Bituminous
☐ Anthracite
☐ Lignite

Accepted by/Affiliation

Date

Relinquished by/Affiliation

Scott J. Birnville / Interpoll Labs Inc.

6/13/94 1000

033094 GASTACK\WPA\FORMSSS-27B.2

INTERPOL LABORATORIES, INC.

(612) 786-6020

Sample Chain of Custody

Job LP-HANWAD Source PROSPTO GUTCH Site STAGE Log No. 2067
 Field Engineer 52 Date of Test 6-8-94 Test No. 2 No. of Runs 3

No. Items	Sample Type	Analysis	Sequence No.	Comments
0	Probe Wash: ☐ DI Water ☐ Acetone ☐ MeCl ₃	☐ EPA M-5 ☐ EPA M-29		
0	Filter: ☐ 4" Glass ☐ 55 Thimble	☐ EPA M-5 ☐ EPA M-29 ☐ EPA M-201A		
5	Impingers: ☐ DI Water ☐ 3% H ₂ O ₂ ☐ 1N NaOH ☐ 2,4-DNPH	☐ MN Protocol ☐ WI Protocol ☐ EPA M-202 ☐ EPA M-6, B ☐ Acid Gases		1 - BLANK 1 - SPINE 3 - 1st Imp 3 - 2nd Imp
3	Integrated Gas: ☒ Tedlar Bag	☐ EPA M-3 ☐ EPA M-10		
0	Oxides of Nitrogen:	☐ EPA M-7A		
0	Fuel Lab: ☐ Fuel Sample	☐ Per S-0163		
0	Particle Sizing:	☐ X-Ray Sculgraph ☐ Cascade Imp		
0	Miscellaneous:	☐		

Fuel Type: Coal: ☐ Bituminous ☐ Anthracite ☐ Lignite
 Oil: ☐ Waste Oil ☐ No. 2 ☐ No. 6
 Misc: ☒ Natural Gas ☐ RDF ☒ S

Relinquished by/Affiliation	Accepted by/Affiliation	Date
<u>David B. Bannell / Fortargols Labs</u>	<u>Robt Long, Fortargols</u>	<u>6/13/94 1000</u>

INTERPOL LABORATORIES, INC.

(612) 786-6020

Sample Chain of Custody

3097

Log No.

Stack

#1 Press 270

Source

LD-HAYWARD

Job

3

No. of Runs

3

Test No.

6-10-94

Date of Test

523

Field Engineer

No. Items	Sample Type	Analysis	Sequence No.	Comments
3	Probe Wash: ☒ Acetone ☐ MeCl ₃	☒ EPA M-5 ☐ EPA M-29		
3	Filter: ☒ 4" Glass ☐ SS Thimble	☒ EPA M-5 ☐ EPA M-29 ☐ EPA M-201A		
3	Impingers: ☒ DI Water ☐ 3% H ₂ O ₂ ☐ 1N NaOH ☐ 2,4-DNPH	☐ IMN Protocol ☒ WI Protocol ☐ EPA M-202 ☐ EPA M-6,8 ☐ Acid Gases		
3	Integrated Gas: ☒ Tedlar Bag	☒ EPA M-3		
0	Oxides of Nitrogen:	☐ EPA M-7A		
1	Fuel Lab: ☒ Fuel Sample	☒ Per 5-0163		
0	Particle Sizing:	☐ X-Ray Sdgraph ☐ Cascade Imp		
0	Miscellaneous:	☐		

Fuel Type: Coal: ☐ Bituminous ☐ Anthracite ☐ Lignite

Wood: ☐ Wood Waste ☐ Dust ☐ Bark

Oil: ☐ Waste Oil ☐ No. 2 ☐ No. 6

Misc: ☒ Natural Gas ☐ RDF

Relinquished by/Affiliation	Accepted by/Affiliation	Date
Don S. Beillo / Interpol Labs Inc.	Bob Seng, Interpol	6/13/94

HOC D

INTERPOL LABORATORIES, INC.

(612) 786-6020

Sample Chain of Custody

Job LP-HAYWARD Source PERFECT OUTLET Site STAG Log No. 3097
 Field Engineer SLB Date of Test 6-7-94 Test No. 3 No. of Runs 3

No. Items	Sample Type	Analysis	Sequence No.	Comments
4	Probe Wash: ☒ DI Water ☐ Acetone ☐ MeCl ₂	☒ EPA M-5 ☐ EPA M-29 ☐ EPA M-201A		
4	Filter: ☒ 4" Glass ☐ SS Thimble	☒ EPA M-5 ☐ EPA M-29 ☐ EPA M-201A		
4	Impingers: ☒ DI Water ☐ 3% H ₂ O ₂ ☐ 1N NaOH ☐ 2,4-DNPH	☐ H ₂ SO ₄ ☐ HNO ₃ /H ₂ O ₂ ☐ KMnO ₄ /H ₂ SO ₄ ☐ Acid Gases		
3	Integrated Gas: ☒ Tedlar Bag	☒ EPA M-3 ☐ EPA M-10		
0	Oxides of Nitrogen:	☐ EPA M-7A ☐ Per S-0163		
0	Fuel Lab: ☐ Fuel Sample	☐ X-Ray Sdgraph ☐ Cascade Imp		
0	Particle Sizing:			
0	Miscellaneous:			

Fuel Type: Coal: ☐ Bituminous ☐ Anthracite ☐ Lignite
 Wood: ☐ Wood Waste ☐ Dust ☐ Bark
 Oil: ☐ Waste Oil ☐ No. 2 ☐ No. 6
 Misc: ☒ Natural Gas ☐ RDF ☐

Relinquished by/Affiliation	Accepted by/Affiliation	Date
Scott Z Bussell/Interpoll Solo Inc.	Scott Z Bussell/Interpoll Solo Inc.	6/13/94

Interpoll Laboratories
(612) 786-6020

SAMPLE CHAIN OF CUSTODY

Job L.P. / Hayward, Ill Source Local Area Site Stack
Field Engineer M. Kaehler Date of Test 6-10-94 Test No. 5 No. of Runs 3

# ITEMS	SAMPLE TYPE	ANALYSIS	LOG NUMBER	COMMENTS
3	Probe Wash: ☒ Acetone ☐ MeCl ₂ ☐ DI Water	☒ EPA M-5 ☐ EPA M-29 ☐ EPA M-201A		
3	Filter: ☐ 4" Glass ☒ 55 Thimble ☐ 2.5" Glass	☒ EPA M-5 ☐ EPA M-29 ☐ EPA M-201A		
3	Impingers: ☒ DI Water ☐ 3% H ₂ O ₂ ☐ 1N NaOH ☐ 2,4-DNPH ☐ H ₂ SO ₄ ☐ HNO ₃ /H ₂ O ₂ ☐ KMnO ₄ /H ₂ SO ₄	☐ IMN Protocol ☒ IAWI Protocol ☐ EPA M-202 ☐ EPA M-6,8 ☐ Acid Gases ☐ IIA Protocol ☐ Formaldehyde ☐ EPA M-29 ☐ EPA M-26		
—	Integrated Gas: ☐ Tedlar Bag	☐ EPA M-3 ☐ EPA M-10		<u>Amberst Air</u>
—	Oxides of Nitrogen:	☐ EPA M-7A ☐		
—	Fuel Lab: ☐ Fuel Sample ☐ Aggregate	☐ Per S-0163		
—	Particle Sizing:	☐ X-Ray Sdgraph ☐ Cascade Imp		
—	Miscellaneous: ☐	☐		

Fuel Type: Coal: ☐ Bituminous ☐ Wood Waste ☐ Oil: ☐ Waste Oil
☐ Anthracite ☐ IDust ☐ No. 2
☐ Lignite ☒ Bark ☐ No. 6

Misc: ☐ Natural Gas
☐ RDF
☐

Relinquished by/Affiliation	Accepted by/Affiliation	Date
<u>Mervin Gochler / Interpoll Labs</u>	<u>B. Song, Interpoll</u>	<u>6/13/94 1000</u>

INTERPOL LABORATORIES, INC.

(612) 786-6020

Sample Chain of Custody

Job Field Engineer LP Hayward Source Green Road Date of Test 6-8-94 Test No. 5 Log No. 3097 No. of Runs 3

Site Stack

Site Stack

Source Green Road

Date of Test 6-8-94

Test No. 5

Log No. 3097

No. of Runs 3

No. Items	Sample Type	Analysis	Sequence No.	Comments
4	Probe Wash: ☒ Acetone ☐ MeCl ₂	☒ EPA M-5 ☐ EPA M-29	☐ EPA M-201A ☐ _____	
4	Filter: ☐ 4" Glass ☒ 55 Thimble	☒ EPA M-5 ☐ EPA M-29 ☐ EPA M-201A	☐ EPA M-17	
4	Impingers: ☒ DI Water ☐ 3% H ₂ O ₂ ☐ 1N NaOH ☐ 2,4-DNPH	☐ MN Protocol ☒ SWI Protocol ☐ EPA M-202 ☐ EPA M-26 ☐ Acid Gases	☐ IIA Protocol ☐ Formaldehyde ☐ EPA M-29 ☐ EPA M-26 ☐ _____	
3	Integrated Gas: ☒ Tedlar Bag	☒ EPA M-3 ☐ _____	☐ EPA M-10	<u>Analyzed on site</u>
12	Oxides of Nitrogen:	☒ EPA M-7A ☐ _____		
	Fuel Lab: ☐ Fuel Sample	☐ Per S-0163		
	Particle Sizing:	☐ X-Ray Sdgraph ☐ _____	☐ Cascade Imp	
	Miscellaneous:	☐ _____		

Fuel Type: Coal: ☐ Bituminous ☐ Anthracite ☐ Lignite
 Wood: ☐ Wood Waste ☐ Dust ☒ Bark
 Oil: ☐ Waste Oil ☐ No. 2 ☐ No. 6
 Misc: ☐ Natural Gas ☐ IRDF ☐ _____

Relinquished by/Affiliation	Accepted by/Affiliation	Date
<u>LP Hayward Interpol</u>	<u>Roby, Interpol</u>	<u>6/13/94 1000</u>

INTERPOLL LABORATORIES, INC.

(612) 786-6020

Sample Chain of Custody

Job CPHAWARD Source WHE/ KANUS Site STACK Log No. 3097
 Field Engineer E THOWHIDGE Date of Test 6-9-94 Test No. 4 No. of Runs

No. Items	Sample Type	Analysis	Sequence No.	Comments
	Probe Wash: ☐ Acetone ☐ MeCl ₂	☐ DI Water ☐	☐ EPA M-5 ☐ EPA M-29 ☐ EPA M-201A	
	Filter: ☐ 4" Glass ☐ SS Thimble	☐ Pallflex ☐ 2.5" Glass	☐ EPA M-5 ☐ EPA M-29 ☐ EPA M-201A	
1 - skip 3	Impingers: ☐ DI Water ☐ 3% H ₂ O ₂ ☐ 1N NaOH ☒ 2,4-DNPH	☐ H ₂ SO ₄ ☐ HNO ₃ /H ₂ O ₂ ☐ KMnO ₄ /H ₂ SO ₄ ☐	☐ JMN Protocol ☒ JWI Protocol ☐ EPA M-202 ☐ EPA M6,8 ☐ Acid Gases ☐ IIA Protocol ☐ Formaldehyde ☐ EPA M-29 ☐ EPA M-26	
3	Integrated Gas: ☒ Tedlar Bag	☐	☒ EPA M-3 ☐ EPA M-7A	
	Oxides of Nitrogen:			
	Fuel Lab: ☐ Fuel Sample	☐ Aggregate	☐ Per S-0163	
	Particle Sizing:		☐ X-Ray Sdgraph ☐	☐ Cascade Imp
	Miscellaneous:	☐	☐	

Fuel Type: Coal: ☐ Bituminous ☐ Anthracite ☐ Lignite
 Wood: ☐ Wood Waste ☐ Dust ☒ Bark
 Oil: ☐ Waste Oil ☐ No. 2 ☐ No. 6
 Misc: ☐ Natural Gas ☐ RDF ☐

Relinquished by/Affiliation	Accepted by/Affiliation	Date
<u>E Thowhidge, Interpoll Labs</u>	<u>Ed Soy, Interpoll</u>	<u>6/13/94 1000</u>

INTERPOL LABORATORIES, INC.

(612) 786-6020

Sample Chain of Custody

Job LP/HAWKSource WHE/KONUSDate of Test 6-9-94Site StackTest No. 7Log No. 3097No. of Runs 3Field Engineer E. T. HAWK

No. Items	Sample Type	Analysis	Sequence No.	Comments
	Probe Wash: ☐ Acetone ☐ MeCl ₃	☐ DI Water ☐ _____	☐ EPA M-5 ☐ EPA M-29	☐ EPA M-201A ☐ _____
	Filter: ☐ 4" Glass ☐ SS Thimble	☐ Pallflex ☐ 2.5" Glass	☐ EPA M-5 ☐ EPA M-29 ☐ EPA M-201A	☐ EPA M-17 ☐ _____
	Impingers: ☐ DI Water ☐ 3% H ₂ O ₂ ☐ 1N NaOH ☐ 2,4-DNPH	☐ H ₂ SO ₄ ☐ HNO ₃ /H ₂ O ₂ ☐ KMnO ₄ /H ₂ SO ₄ ☐ _____	☐ MN Protocol ☐ WI Protocol ☐ EPA M-202 ☐ EPA M-6, B ☐ Acid Gases	☐ IA Protocol ☐ Formaldehyde ☐ EPA M-29 ☐ EPA M-26 ☐ _____
	Integrated Gas: ☐ Tedlar Bag	☐ _____	☐ EPA M-3 ☐ _____	☐ EPA M-10 ☐ _____
	Oxides of Nitrogen:		☐ EPA M-7A ☐ _____	☐ _____
	Fuel Lab: ☐ Fuel Sample	☐ Aggregate	☐ Per S-0163	☐ _____
	Particle Sizing:		☐ X-Ray Sdgraph ☐ _____	☐ Cascade Imp ☐ _____
<u>6</u>	Miscellaneous:	☐ _____	☐ _____	☐ _____

Fuel Type: Coal: ☐ Bituminous ☐ Wood Waste ☐ Oil: ☐ Waste Oil ☐ Natural Gas
☐ Anthracite ☐ No. 2 ☐ IRDF
☐ Lignite ☐ No. 6 ☐

Relinquished by/Affiliation	Accepted by/Affiliation	Date
<u>E. T. Hawk / Interpol Lab</u>	<u>Ed. S. J. / Interpol</u>	<u>6/13/94 1000</u>

INTERPOL LABORATORIES, INC.

(612) 786-6020

Sample Chain of Custody

Log No. 3097
No. of Runs 5

Source LINE / KONES

Date of Test 6-9-94

Test No. 9

Job CP/HAYWARD
Field Engineer E. THOMAS

No. Items	Sample Type	Analysis	Sequence No.	Comments
	Probe Wash: ☐ Acetone ☐ MeCl ₃	☐ DI Water ☐ _____	☐ EPA M-5 ☐ EPA M-29	☐ EPA M-201A ☐ _____
	Filter: ☐ 4" Glass ☐ SS Thimble	☐ Pallflex ☐ 2.5" Glass	☐ EPA M-5 ☐ EPA M-29 ☐ EPA M-201A	☐ EPA M-17
	Impingers: ☐ DI Water ☐ 3% H ₂ O ₂ ☐ 1N NaOH ☐ 2,4-DNPH	☐ H ₂ SO ₄ ☐ HNO ₃ /H ₂ O ₂ ☐ KMnO ₄ /H ₂ SO ₄ ☐ _____	☐ MN Protocol ☐ WI Protocol ☐ EPA M-202 ☐ EPA M-6,8 ☐ Acid Gases	☐ IA Protocol ☐ Formaldehyde ☐ EPA M-29 ☐ EPA M-26 ☐ _____
	Integrated Gas: ☐ Tedlar Bag	☐ _____	☐ EPA M-3 ☐ _____	☐ EPA M-10
	Oxides of Nitrogen:		☐ EPA M-7A ☐ _____	
	Fuel Lab: ☐ Fuel Sample	☐ Aggregate	☐ Per S-0163	
	Particle Sizing:		☐ X-Ray Sdgraph ☐ Cascade Imp	
<u>6</u>	Miscellaneous:	☒ <u>BITUMINOUS</u>	☒ <u>BENZENE</u>	

Fuel Type: Coal: ☐ Bituminous ☐ Anthracite ☐ Lignite
Wood: ☐ Wood Waste ☐ Dust ☒ Bark
Oil: ☐ Waste Oil ☐ No. 2 ☐ No. 6
Misc: ☐ Natural Gas ☐ RDF ☐ _____

Relinquished by/Affiliation <u>E. Thomas - INTERPOL Lab</u>	Accepted by/Affiliation <u>Bobey, J. Popol</u>	Date <u>6/13/94 1000</u>
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033094-G:1STACK\WP\FORMS\5-27B.2

INTERPOL LABORATORIES, INC.

(612) 786-6020

Sample Chain of Custody

Job Field Engineer 6.12.1 Hayward, WI Source Line 1 Kerosene Site Stack Log No. 30977
M. Haeckler Date of Test 6-9-94 Test No. 8 No. of Runs 3

No. Items	Sample Type	Analysis	Sequence No.	Comments
3+1	Probe Wash: ☒ Acetone ☒ MeCl ₄	☐ DI Water ☐ _____	☐ EPA M-5 ☐ EPA M-29	☐ EPA M-201A ☒ POM
3+1	Filter: ☒ 2" Glass ☐ SS Thimble	☐ Pallflex ☐ 2.5" Glass	☐ EPA M-5 ☐ EPA M-29 ☐ EPA M-201A	☐ EPA M-17 ☒ POM
3+1	Impingers: ☒ DI Water ☐ 3% H ₂ O ₂ ☐ 1N NaOH ☐ 2,4-DNPH	☐ H ₂ SO ₄ ☐ HNO ₃ /H ₂ O ₂ ☐ KMnO ₄ /H ₂ SO ₄ ☐ _____	☐ IMN Protocol ☐ WI Protocol ☐ EPA M-202 ☐ EPA M-26 ☐ Acid Gases	☐ IIA Protocol ☐ Formaldehyde ☐ EPA M-29 ☐ EPA M-26 ☒ POM
3	Integrated Gas: ☐ Tedlar Bag	☐ _____	☒ EPA M-3 ☐ _____	☐ EPA M-10
—	Oxides of Nitrogen:		☐ EPA M-7A ☐ _____	
—	Fuel Lab: ☐ Fuel Sample	☐ Aggregate	☐ Per S-0163	
—	Particle Sizing:		☐ X-Ray Sdgraph ☐ _____	☐ Cascade Imp
—	Miscellaneous:	☐ _____	☐ _____	

Fuel Type: Coal: ☐ Bituminous ☐ Anthracite ☐ Lignite
 Wood: ☐ Wood Waste ☐ Dust ☒ Bark
 Oil: ☐ Waste Oil ☐ No. 2 ☐ No. 6
 Misc: ☐ Natural Gas ☐ RDF ☐ _____

Relinquished by/Affiliation	Accepted by/Affiliation	Date
<u>Mark Haeckler / Interpoll Labs</u>	<u>M. Haeckler, Interpoll</u>	<u>6/13/94 1000</u>

INTERPOL LABORATORIES, INC.

(612) 786-6020

Sample Chain of Custody

Job Field Engineer L.P. Hayward Source Lin 2 Press Vent Site R70 Stack Log No. 3097
2/10/94 Date of Test 6/10/94 Test No. 12 No. of Runs 3

No. Items	Sample Type	Analysis	Sequence No.	Comments
	Probe Wash: ☐ DI Water ☐ Acetone ☐ MeCl ₂	☐ EPA M-5 ☐ EPA M-29 ☐ EPA M-201A		
	Filters: ☐ 4" Glass ☐ 55 Thimble	☐ EPA M-5 ☐ EPA M-29 ☐ EPA M-201A		
5	Impingers: ☐ DI Water ☐ 3% H ₂ O ₂ ☐ 1N NaOH ☒ 2,4-DNPH	☐ IMN Protocol ☐ IWI Protocol ☐ EPA M-202 ☐ EPA M-6, 8 ☐ Acid Gases ☒ IA Protocol ☐ Formaldehyde ☐ EPA M-29 ☐ EPA M-26 ☒ 2011		<u>L.P. Hayward</u> <u>3 sample runs</u>
	Integrated Gas: ☐ Tedlar Bag	☐ EPA M-3 ☐ EPA M-10		
	Oxides of Nitrogen:	☐ EPA M-7A ☐ EPA M-163		
	Fuel Lab: ☐ Fuel Sample	☐ X-Ray Scdgraph ☐ Cascade Imp		
	Particle Sizing:			
	Miscellaneous:			

Fuel Type: Coal: ☐ Bituminous ☐ Anthracite ☐ Lignite
 Wood: ☐ Wood Waste ☐ Dust ☐ Bark
 Oil: ☐ Waste Oil ☐ No. 2 ☐ No. 6
 Misc: ☐ Natural Gas ☐ RDF ☐

Relinquished by/Affiliation	Accepted by/Affiliation	Date
<u>Dan Van Haver</u>		

INTERPOL LABORATORIES, INC.
(612) 786-6020

Sample Chain of Custody

Job L.P. Hayward Source Line 2 Press Date of Test 6/9/94 Test No. 13 Log No. 3097
Field Engineer DW No. of Runs 3

No. Items	Sample Type	Analysis	Sequence No.	Comments
	Probe Wash: ☐ Acetone ☐ MeCl ₂	☐ DI Water ☐ _____	☐ EPA M-5 ☐ EPA M-29	☐ EPA M-201A ☐ _____
	Filters: ☐ 4" Glass ☐ SS Thimble	☐ Pallflex ☐ 2.5" Glass	☐ EPA M-5 ☐ EPA M-29 ☐ EPA M-201A	☐ EPA M-17
5	Impingers: ☐ DI Water ☐ 3% H ₂ O ₂ ☐ 1N NaOH ☐ 2,4-DNPH	☐ H ₂ SO ₄ ☐ HNO ₃ /H ₂ O ₂ ☐ KMnO ₄ /H ₂ SO ₄ ☒ 1-2 PP IN TOLUENE	☐ IMN Protocol ☐ WI Protocol ☐ EPA M-202 ☐ EPA M-26 ☐ Acid Gases	☐ IA Protocol ☐ Formaldehyde ☐ EPA M-29 ☐ EPA M-26 ☒ MDE
	Integrated Gas: ☐ Tedlar Bag	☐ _____	☐ EPA M-3 ☐ _____	☐ EPA M-10
	Oxides of Nitrogen:		☐ EPA M-7A ☐ _____	
	Fuel Lab: ☐ Fuel Sample	☐ Aggregate	☐ Per S-0163	
	Particle Sizing:		☐ X-Ray Scatgraph ☐ _____	☐ Cascade Imp
	Miscellaneous:	☐ _____		

Fuel Type: Coal: ☐ Bituminous ☐ Anthracite ☐ Lignite
Oil: ☐ Waste Oil ☐ No. 2 ☐ No. 6
Misc: ☐ Natural Gas ☐ RDF ☐ _____

Relinquished by/Affiliation	Accepted by/Affiliation	Date
<u>Deane Van Haver</u>		<u>6/9/94</u>

INTERPOL LABORATORIES, INC.

(612) 786-6020

Sample Chain of Custody

Job L.P. Hayward Source Line 2 Pressurized Log No. 3097
 Field Engineer Dust Date of Test 6/9/94 Test No. 13 No. of Runs 3

No. Items	Sample Type	Analysis	Sequence No.	Comments
	Probe Wash: ☐ Acetone ☐ MeCl ₂	☐ EPA M-5 ☐ EPA M-29		
	Filter: ☐ 4" Glass ☐ 55 Thimble	☐ EPA M-5 ☐ EPA M-29 ☐ EPA M-201A		
5	Impingers: ☐ DI Water ☐ 3% H ₂ O ₂ ☐ 1N NaOH ☐ 2,4-DNPH	☐ MN Protocol ☐ WI Protocol ☐ EPA M-202 ☐ EPA M-6,8 ☐ Acid Gases		1 Blank 1 Spike 3 1st impinger 3 2nd impinger
	Integrated Gas: ☐ Tedlar Bag	☐ EPA M-3 ☐		
	Oxides of Nitrogen:	☐ EPA M-7A ☐		
	Fuel Labr: ☐ Fuel Sample	☐ Per 5-0163		
	Particle Sizing:	☐ X-Ray Scigraph ☐		
	Miscellaneous: ☐	☐		

Fuel Type: Coal: ☐ Bituminous ☐ Anthracite ☐ Lignite
 Wood: ☐ Wood Waste ☐ Dust ☐ Bark
 Oil: ☐ Waste Oil ☐ No. 2 ☐ No. 6
 Misc: ☐ Natural Gas ☐ RDF ☐

Relinquished by/Affiliation	Accepted by/Affiliation	Date
<u>Deane Van Haver</u>	<u>Bob Say, Interpol</u>	<u>6/9/94 1000</u>

INTERPOL LABORATORIES, INC.

(612) 786-6020

Sample Chain of Custody

Job Field Engineer L.P. HARWARD Source Line 2 Dwyer Date of Test 6/8/84 Site RTO STACK Log No. 3097 No. of Runs 3

No. Items	Sample Type	Analysis	Sequence No.	Comments
4	Probe Wash: ☒ Acetone ☐ MeCl ₂	☒ EPA M-5 ☐ EPA M-29	☐ EPA M-201A ☐ _____	
4	Filter: ☐ 4" Glass ☐ SS Thimble	☒ EPA M-5 ☐ EPA M-29 ☐ EPA M-201A	☐ EPA M-17 ☐ _____	
4	Impingers: ☒ DI Water ☐ 3% H ₂ O ₂ ☐ 1N NaOH ☐ 2,4-DNPH	☐ IMN Protocol ☒ XWI Protocol ☐ EPA M-202 ☐ EPA M6,8 ☐ Acid Gases	☐ IA Protocol ☐ Formaldehyde ☐ EPA M-29 ☐ EPA M-26 ☐ _____	
3	Integrated Gas: ☒ Tedlar Bag	☒ EPA M-3 ☐ _____	☐ EPA M-10 ☐ _____	
	Oxides of Nitrogen:	☐ EPA M-7A ☐ _____		
	Fuel Lab: ☐ Fuel Sample	☐ Per S-0163		
	Particle Sizing:	☐ X-Ray Scdgraph ☐ _____	☐ Cascade Imp ☐ _____	
	Miscellaneous:	☐ _____		

Fuel Type: Coal: ☐ Bituminous ☐ Anthracite ☐ Lignite
Wood: ☐ Wood Waste ☐ Dust ☐ Bark
Oil: ☐ Waste Oil ☐ No. 2 ☐ No. 6
Misc: ☐ Natural Gas ☐ RDF ☐ _____

Relinquished by/Affiliation	Accepted by/Affiliation	Date
<u>Deane Van Poy</u>		

INTERPOLL LABORATORIES, INC.

(612) 786-6020

Sample Chain of Custody

Job L.P. HAYWARD Source Linc 2 DRYER Site RTO STACK Log No. 3097
 Field Engineer DVT Date of Test 6/9/94 Test No. 14 No. of Runs 3

No. Items	Sample Type	Analysis	Sequence No.	Comments
4	Probe Wash: ☒ Acetone ☐ MeCl ₃	☒ EPA M-5 ☐ EPA M-29		
4	Filters: ☐ 4" Glass ☐ 55 Thimble	☒ EPA M-5 ☐ EPA M-29 ☐ EPA M-201A		
4	Impingers: ☒ DI Water ☐ 3% H ₂ O ₂ ☐ 1N NaOH ☐ 12.4-DNPH	☐ MN Protocol ☒ MWI Protocol ☐ EPA M-202 ☐ EPA M6,0 ☐ Acid Gases		
3	Integrated Gas: ☒ Tedlar Bag	☒ EPA M-3 ☐ EPA M-10		
	Oxides of Nitrogen:	☐ EPA M-7A		
	Fuel Lab: ☐ Fuel Sample	☐ Per S-0163		
	Particle Sizing:	☐ X-Ray Sdgraph ☐ Cascade Imp		
	Miscellaneous:	☐		

Fuel Type: Coal: ☐ Bituminous ☐ Anthracite ☐ Lignite
 Wood: ☐ Wood Waste ☐ Dust ☐ Bark
 Oil: ☐ Waste Oil ☐ No. 2 ☐ No. 6
 Misc: ☐ Natural Gas ☐ RDF ☐

Relinquished by/Affiliation	Accepted by/Affiliation	Date
<u>Dwayne Van Housen</u>	<u>Bob Berg, Interpoll</u>	<u>6/13/94 1000</u>

INTERPOLLAB LABORATORIES, INC.

(612) 786-6020

Sample Chain of Custody

Job Field Engineer L.P. Haywood, Jr. Source Line 3 Boilers Site Stack Log No. 3097
Michael Date of Test 6-8-94 Test No. 16 No. of Runs 3

No. Items	Sample Type	Analysis	Sequence No.	Comments
3	Probe Wash: ☒ Acetone ☐ MeCl ₂ ☐ DI Water	☒ EPA M-5 ☐ EPA M-29	☐ EPA M-201A	
3	Filter: ☐ 4" Glass ☒ SS Thimble	☒ EPA M-5 ☐ EPA M-29 ☐ EPA M-201A	☐ EPA M-17	
3	Impingers: ☒ DI Water ☐ 3% H ₂ O ₂ ☐ 1N NaOH ☐ 2,4-DNPH	☐ MN Protocol ☒ SAWI Protocol ☐ EPA M-202 ☐ EPA M6,8 ☐ Acid Cases	☐ IIA Protocol ☐ Formaldehyde ☐ EPA M-29 ☐ EPA M-26	
3	Integrated Gas: ☒ Tedlar Bag	☒ EPA M-3	☒ EPA M-10	Analyzed in Field
12	Oxides of Nitrogen:	☒ EPA M-7A		
—	Fuel Lab: ☐ Fuel Sample	☐ Per S-0163		
—	Particle Sizing:	☐ X-Ray Sdgraph	☐ Cascade Imp	
—	Miscellaneous:	☐		

Fuel Type: Coal: ☐ Bituminous ☐ Wood Waste ☐ Oil: ☐ Waste Oil ☐ Natural Gas
☐ Anthracite ☐ Dust ☐ No. 2 ☐ RDF
☐ Lignite ☒ Bark ☐ No. 6

Relinquished by/Affiliation	Accepted by/Affiliation	Date
Mark Gaebler / Interpoll Labs	Michael, Jr. Haywood	6/13/94

INTERPOL LABORATORIES, INC.

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Sample Chain of Custody

Job Field Engineer L.P. / Hayward Source Line 2 Keros Site Stack Log No. 3097
Mr. Kaehler Date of Test 6-8-94 Test No. 17 No. of Runs 3

No. Items	Sample Type	Analysis	Sequence No.	Comments
3+1	Probe Wash: ☐ Acetone ☒ MeCl ₂	☐ DI Water ☐ _____	☐ EPA M-5 ☐ EPA M-29 ☐ EPA M-201A	<u>Added to Impinger</u>
—	Filter: ☐ 4" Glass ☐ SS Thimble	☐ Pallflex ☐ 2.5" Glass	☐ EPA M-5 ☐ EPA M-29 ☐ EPA M-201A	
3+1	Impingers: ☐ DI Water ☐ 3% H ₂ O ₂ ☐ 1N NaOH ☒ 2,4-DNPH	☐ H ₂ SO ₄ ☐ HNO ₃ /H ₂ O ₂ ☐ KMnO ₄ /H ₂ SO ₄ ☐ _____	☐ IMN Protocol ☐ WI Protocol ☐ EPA M-202 ☐ EPA M-6,8 ☐ Acid Gases ☐ I/A Protocol ☒ Formaldehyde ☐ EPA M-29 ☐ EPA M-26 ☐ _____	
3	Integrated Gas: ☐ Tedlar Bag	☐ _____	☒ EPA M-3 ☐ _____ ☐ EPA M-7A ☐ _____ ☐ Per S-0163	<u>Analyzed in Field</u>
—	Oxides of Nitrogen:			
—	Fuel Lab: ☐ Fuel Sample	☐ Aggregate		
—	Particle Sizing:		☐ X-Ray Sdgraph ☐ _____ ☐ Cascade Imp	
—	Miscellaneous:	☐ _____		

Fuel Type: Coal: ☐ Bituminous ☐ Anthracite ☐ Lignite
 Wood: ☐ Wood Waste ☐ Dust ☒ Bark
 Oil: ☐ Waste Oil ☐ No. 2 ☐ No. 6
 Misc: ☐ Natural Gas ☐ RDF ☐ _____

Relinquished by/Affiliation	Accepted by/Affiliation	Date
<u>Mark Kaehler / Interpol Labs</u>	<u>Bob Sany, Interpol</u>	<u>6/13/94 1000</u>

INTERPOLL LABORATORIES, INC.

(612) 786-6020

Sample Chain of Custody

Job L.P. / Hayward, IL Source Line 2 / Leaks Site Stuck Log No. 3097
 Field Engineer M. Kachler Date of Test 6-8-94 Test No. 18 No. of Runs 3

No. Items	Sample Type	Analysis	Sequence No.	Comments
—	Probe Wash: ☐ Acetone ☐ MeCl ₃	☐ DI Water ☐ _____		
—	Filter: ☐ 4" Glass ☐ SS Thimble	☐ Pallflex ☐ 2.5" Glass		
3+3	Impingers: ☐ DI Water ☐ 3% H ₂ O ₂ ☐ 1N NaOH ☐ 2,4-DNPH	☐ H ₂ SO ₄ ☐ HNO ₃ /H ₂ O ₂ ☐ KMnO ₄ /H ₂ SO ₄ ☒ A+B Phenol		
✓	Integrated Gas: ☐ Tedlar Bag	☐ _____		Simultaneously with CH ₄ O
—	Oxides of Nitrogen:	☐ EPA M-3 ☐ EPA M-7A ☐ _____		
—	Fuel Lab: ☐ Fuel Sample	☐ Per S-0163		
—	Particle Sizing:	☐ X-Ray Scdgraph ☐ Cascade Imp ☐ _____		
—	Miscellaneous: ☐ _____	☐ _____		

Fuel Type: Coat: ☐ Bituminous ☐ Anthracite ☐ Lignite
 Wood: ☐ Wood Waste ☐ Dust ☒ Bark
 Oil: ☐ Waste Oil ☐ No. 2 ☐ No. 6
 Misc: ☐ Natural Gas ☐ RDF ☐ _____

Relinquished by/Affiliation	Accepted by/Affiliation	Date
<u>Mark Gachler / Interpoll Labs</u>	<u>M. Kachler, Interpoll</u>	<u>6/13/94 1000</u>

INTERPOLL LABORATORIES, INC.

(612) 786-6020

Sample Chain of Custody

Job Field Engineer W. Kachala Source Line 2 / Hwy / St. 111 Date of Test 6-7-94 Test No. 19 Log No. 3097 No. of Runs 3

No. Items	Sample Type	Analysis	Sequence No.	Comments
3+1	Probe Wash: ☒ DI Water ☒ Acetone ☒ MeCl ₂	☐ DI Water ☐ EPA M-5 ☐ EPA M-29 ☐ EPA M-201A		
3+1	Filter: ☒ 4" Glass ☐ SS Thimble	☐ Pallflex ☐ 2.5" Glass ☐ EPA M-5 ☐ EPA M-17 ☐ EPA M-29 ☐ EPA M-201A		
3+1	Impingers: ☒ DI Water ☐ 3% H ₂ O ₂ ☐ 1N NaOH ☐ 2,4-DNPH	☐ H ₂ SO ₄ ☐ HNO ₃ /H ₂ O ₂ ☐ KMnO ₄ /H ₂ SO ₄ ☐ Acid Gases ☐ MN Protocol ☐ WI Protocol ☐ EPA M-202 ☐ EPA M-6,8 ☐ EPA M-26 ☐ EPA M-10		
3	Integrated Gas: ☒ Tedlar Bag	☐ EPA M-3 ☐ EPA M-7A		
-	Oxides of Nitrogen:	☐ Per 5-0163		
-	Fuel Lab: ☐ Fuel Sample	☐ X-Ray Scigraph ☐ Cascade Imp		
-	Particle Sizing:			
-	Miscellaneous:			

Fuel Type: Coal: ☐ Bituminous ☐ Anthracite ☐ Lignite
Oil: ☐ Waste Oil ☐ No. 2 ☐ No. 6
Misc: ☐ Natural Gas ☐ RDF ☐

Relinquished by/Affiliation	Accepted by/Affiliation	Date
<u>Mark G. Anderson / Interpoll Labs</u>	<u>W. Kachala / Interpoll Labs</u>	<u>6/12/94 1000</u>

033094-G:STACKWIPFORMSS-27B.2

Interpoll Laboratories
(612) 786-6020

SAMPLE CHAIN OF CUSTODY

Job L.S. / Hayward, Ill Source Line 2 Run Site Staub
Field Engineer M. Gachler Date of Test 6-7-94 Test No. 20 No. of Runs 3

# ITEMS	SAMPLE TYPE	ANALYSIS	LOG NUMBER	COMMENTS
-	Probe Wash: ☐ Acetone ☐ MeCl ₂	☐ DI Water ☐ _____	☐ EPA M-5 ☐ EPA M-29	☐ EPA M-201A ☐ _____
-	Filter: ☐ 4" Glass ☐ SS Thimble	☐ Pallflex ☐ 2.5" Glass	☐ EPA M-5 ☐ EPA M-29 ☐ EPA M-201A	☐ EPA M-17 _____ _____ _____
3	Impingers: ☐ DI Water ☐ 3% H ₂ O ₂ ☐ 1N NaOH ☐ 2,4-DNPH	☐ H ₂ SO ₄ ☐ HNO ₃ /H ₂ O ₂ ☐ KMnO ₄ /H ₂ SO ₄ ☒ Charcoal Tubes	☐ MN Protocol ☐ WI Protocol ☐ EPA M-202 ☐ EPA M-6,8 ☐ Acid Gases	☐ IIA Protocol ☐ Formaldehyde ☐ EPA M-29 ☐ EPA M-26 ☒ Benzene
✓	Integrated Gas: ☐ Tedlar Bag	☐ _____	☐ EPA M-3 ☐ _____	☐ EPA M-10 Done during PM-10 testing
-	Oxides of Nitrogen:		☐ EPA M-7A ☐ _____	_____ _____ _____
-	Fuel Lab: ☐ Fuel Sample	☐ Aggregate	☐ Per S-0163	_____ _____ _____
-	Particle Sizing:		☐ X-Ray Sdgraph ☐ _____	☐ Cascade Imp _____ _____ _____
-	Miscellaneous:	☐ _____	☐ _____	_____ _____ _____

Fuel Type: Coal: ☐ Bituminous ☐ Wood Waste ☐ Oil: ☐ Waste Oil ☐ Natural Gas
☐ Anthracite ☐ Dust ☐ No. 2 ☐ RDF
☐ Lignite ☒ Bark ☐ No. 6 ☐

Relinquished by/Affiliation	Accepted by/Affiliation	Date
M. Gachler / Interpoll Labs	M. Gachler / Interpoll	6/13/94

INTERPOL LABORATORIES, INC.

(612) 786-6020

Sample Chain of Custody

Job LP - MAYWOOD Source 02 Press RTD Site INLET Log No. 3097
 Field Engineer SIB Date of Test 6-8-94 Test No. 21 No. of Runs 9

No. Items	Sample Type	Analysis	Sequence No.	Comments
4	Probe Wash: ☒ Acetone ☐ MeCl ₂	☒ EPA M-5 ☐ EPA M-29		
4	Filler: ☐ 4" Glass ☐ SS Thimble	☒ EPA M-5 ☐ EPA M-29 ☐ EPA M-201A		
4	Impingers: ☒ DI Water ☐ 3% H ₂ O ₂ ☐ 1N NaOH ☐ 2,4-DNPH	☐ IAN Protocol ☒ IAWI Protocol ☐ EPA M-202 ☐ EPA M-6,8 ☐ Acid Gases		
0	Integrated Gas: ☐ Tedlar Bag	☐ EPA M-3		Online Air
0	Oxides of Nitrogen:	☐ EPA M-7A		
0	Fuel Lab: ☐ Fuel Sample	☐ Per S-0163		
0	Particle Sizing:	☐ X-Ray Silgraph ☐ Cascade Imp		
0	Miscellaneous:	☐		

Fuel Type: Coal: ☐ Bituminous ☐ Anthracite ☐ Lignite
 Wood: ☐ Wood Waste ☐ Dust ☐ Bark
 Oil: ☐ Waste Oil ☐ No. 2 ☐ No. 6
 Misc: ☐ Natural Gas ☐ RDF ☒ *Lab test Air*

Relinquished by/Affiliation	Accepted by/Affiliation	Date
<i>Robert S. C. A. / Interpoll Lab</i>	<i>Bob S. / Interpoll</i>	<i>6/13/94 1000</i>

INTERPOL LABORATORIES, INC.

(612) 786-6020

Sample Chain of Custody

Job L.P. Hayward Source Lin 2 Press Vent Site RTO Stack Log No. 3097
 Field Engineer Deirdre Date of Test 6/10/94 Test No. 3 No. of Runs 3

No. Items	Sample Type	Analysis	Sequence No.	Comments
	Probe Wash: ☐ Acetone ☐ MeCl ₃	☐ EPA M-5 ☐ EPA M-29	☐ EPA M-201A ☐ _____	
	Filters: ☐ 4" Glass ☐ 55 Thimble	☐ EPA M-5 ☐ EPA M-29 ☐ EPA M-201A	☐ EPA M-17	
5	Impingers: ☐ DI Water ☐ 3% H ₂ O ₂ ☐ 1N NaOH ☒ 2,4-DNPH	☐ MN Protocol ☐ WI Protocol ☐ EPA M-202 ☐ EPA M-6,8 ☐ Acid Gases	☐ IA Protocol ☐ Formaldehyde ☐ EPA M-29 ☐ EPA M-26 ☒ 2011	<u>1. Blank</u> <u>1. Spike</u> <u>3 sample runs</u>
	Integrated Gas: ☐ Tedlar Bag	☐ EPA M-3 ☐ _____	☐ EPA M-10	
	Oxides of Nitrogen:	☐ EPA M-7A ☐ _____		
	Fuel Lab: ☐ Fuel Sample	☐ Per S-0163		
	Particle Sizing:	☐ X-Ray Scatgraph ☐ _____	☐ Cascade Imp	
	Miscellaneous: ☐ _____	☐ _____		

Fuel Type: Coal: ☐ Bituminous ☐ Anthracite ☐ Lignite
 Wood Waste: ☐ Wood Waste ☐ Dust ☐ Bark
 Oil: ☐ No. 2 ☐ No. 6
 Misc: ☐ Natural Gas ☐ RDF ☐ _____

Relinquished by/Affiliation	Accepted by/Affiliation	Date
<u>Diane Van Haver</u>	<u>Bobby, DePaul</u>	<u>6/13/94 1000</u>

APPENDIX F

TOTAL HYDROCARBONS STRIPCHARTS / DATA LOGGER PRINTOUTS

Interpoll Laboratories, Inc.
(612) 786-6020

Printout of ESC Model 80 DAS
for CEM Trailer No. 1
- 1994 -

File Name: LPH14
Job Number: 4-3097
Client: Louisiana Pacific Corporation
Location: Hayward, Wisconsin

Line 1 Press RTO Outlet Stack -- Run 1

Julian Date	Time (Hrs)	Conc. (dry basis unless noted)			
		NOx (ppmv)	CO (ppmv)	CO2 (%v/v)	O2 (%v/v)
161	09:36:00	22.4	16.2	1.00	20.32
161	09:37:00	28.3	27.7	0.43	20.28
161	09:38:00	20.9	16.2	0.39	20.30
161	09:39:00	22.9	15.5	0.40	20.29
161	09:40:00	27.6	26.7	0.39	20.34
161	09:41:00	21.5	18.7	0.41	20.24
161	09:42:00	22.5	14.8	0.38	20.32
161	09:43:00	27.7	24.6	0.39	20.33
161	09:44:00	23.1	21.2	0.43	20.25
161	09:45:00	22.4	14.9	0.39	20.29
161	09:46:00	27.8	21.5	0.37	20.35
161	09:47:00	23.2	23.7	0.43	20.24
161	09:48:00	22.2	14.3	0.39	20.31
161	09:49:00	27.9	19.1	0.38	20.30
161	09:50:00	23.9	26.3	0.41	20.30
161	09:51:00	22.2	14.7	0.38	20.29
161	09:52:00	28.3	18.6	0.41	20.28
161	09:53:00	24.5	26.8	0.37	20.34
161	09:54:00	23.0	15.6	0.42	20.23
161	09:55:00	27.4	18.4	0.40	20.29
161	09:56:00	26.2	25.3	0.38	20.32
161	09:57:00	23.5	16.9	0.42	20.25
161	09:58:00	26.5	18.1	0.40	20.28
161	09:59:00	27.6	23.3	0.35	20.36
161	10:00:00	22.7	19.5	0.41	20.26
161	10:01:00	25.8	16.6	0.39	20.32
161	10:02:00	29.3	22.6	0.39	20.28
161	10:03:00	22.0	20.8	0.39	20.33
161	10:04:00	24.3	15.2	0.38	20.29
161	10:05:00	30.0	22.3	0.40	20.30
161	10:06:00	20.8	22.0	0.35	20.36
161	10:07:00	21.3	14.1	0.42	20.23
161	10:08:00	20.7	11.4	0.41	20.25
161	10:09:00	20.3	10.5	0.41	20.26

Interpoll Laboratories, Inc.
(612) 786-6020

Printout of ESC Model 80 DAS
for CEM Trailer No. 1
- 1994 -

File Name: LPH14
Job Number: 4-3097
Client: Louisiana Pacific Corporation
Location: Hayward, Wisconsin

Line 1 Press RTO Outlet Stack -- Run 1

Julian Date	Time (Hrs)	Conc. (dry basis unless noted)			
		NOx (ppmv)	CO (ppmv)	CO2 (%v/v)	O2 (%v/v)
161	10:10:00	21.5	10.1	0.43	20.20
161	10:11:00	20.9	9.3	0.41	20.24
161	10:12:00	19.7	8.8	0.37	20.29
161	10:13:00	21.4	10.2	0.43	20.22
161	10:14:00	27.3	15.6	0.41	20.27
161	10:15:00	28.7	20.0	0.42	20.21
161	10:16:00	21.0	15.3	0.39	20.31
161	10:17:00	23.8	12.6	0.39	20.26
161	10:18:00	31.2	19.8	0.45	20.22
161	10:19:00	21.7	18.4	0.38	20.29
161	10:20:00	23.9	13.7	0.43	20.22
161	10:21:00	30.9	19.4	0.42	20.26
161	10:22:00	22.4	17.9	0.38	20.31
161	10:23:00	23.1	14.0	0.41	20.24
161	10:24:00	29.6	18.7	0.42	20.26
161	10:25:00	22.9	16.9	0.36	20.30
161	10:26:00	22.5	14.6	0.41	20.26
161	10:27:00	28.6	17.5	0.41	20.28
161	10:28:00	26.3	18.5	0.48	20.14
161	10:29:00	23.9	13.8	0.50	20.12
161	10:30:00	29.1	13.8	0.49	20.08
161	10:31:00	31.2	16.4	0.57	20.03
161	10:32:00	24.1	11.5	0.50	20.08
161	10:33:00	30.0	12.1	0.55	20.02
161	10:34:00	32.4	14.2	0.53	20.05
161	10:35:00	24.8	9.6	0.52	20.07
161	10:36:00	29.2	10.6	0.53	20.03
Run Average		25.0	17.2	0.43	20.25

Interpoll Laboratories, Inc.
(612) 786-6020

Printout of ESC Model 80 DAS
for CEM Trailer No. 1
- 1994 -

File Name: LPH15
Job Number: 4-3097
Client: Louisiana Pacific Corporation
Location: Hayward, Wisconsin

Line 1 Press RTO Outlet Stack -- Run 2

Julian Date	Time (Hrs)	Conc. (dry basis unless noted)			
		NOx (ppmv)	CO (ppmv)	CO2 (%v/v)	O2 (%v/v)
161	11:01:00	9.5	7.1	0.47	20.07
161	11:02:00	13.2	9.1	0.49	20.06
161	11:03:00	20.6	10.5	0.54	19.98
161	11:04:00	11.3	9.3	0.46	20.10
161	11:05:00	12.3	7.2	0.49	20.05
161	11:06:00	19.2	12.0	0.48	20.10
161	11:07:00	13.8	12.3	0.53	20.00
161	11:08:00	12.7	7.4	0.51	20.00
161	11:09:00	20.1	10.6	0.51	20.04
161	11:10:00	14.0	8.7	0.48	20.05
161	11:11:00	12.0	8.7	0.47	20.06
161	11:12:00	19.3	9.4	0.53	20.00
161	11:13:00	17.0	11.1	0.47	20.08
161	11:14:00	12.4	7.6	0.48	20.04
161	11:15:00	16.7	9.8	0.44	20.12
161	11:16:00	20.2	12.6	0.53	19.99
161	11:17:00	13.3	7.5	0.50	20.00
161	11:18:00	17.0	9.4	0.47	20.08
161	11:19:00	20.0	9.2	0.47	20.05
161	11:20:00	12.4	9.6	0.45	20.09
161	11:21:00	17.4	8.6	0.51	20.00
161	11:22:00	22.8	11.2	0.48	20.05
161	11:23:00	13.7	9.5	0.49	20.01
161	11:24:00	13.2	7.4	0.44	20.10
161	11:25:00	23.9	12.0	0.52	20.01
161	11:26:00	16.6	10.2	0.50	19.99
161	11:27:00	13.5	8.5	0.44	20.11
161	11:28:00	20.7	8.9	0.47	20.05
161	11:29:00	16.7	13.4	0.45	20.08
161	11:30:00	14.2	8.9	0.48	20.01
161	11:31:00	19.2	9.6	0.45	20.05
161	11:32:00	19.0	12.0	0.49	20.03
161	11:33:00	12.1	7.1	0.42	20.10
161	11:34:00	18.2	10.0	0.48	20.06

Interpoll Laboratories, Inc.
(612) 786-6020

Printout of ESC Model 80 DAS
for CEM Trailer No. 1
- 1994 -

File Name: LPH15
Job Number: 4-3097
Client: Louisiana Pacific Corporation
Location: Hayward, Wisconsin

Line 1 Press RTO Outlet Stack -- Run 2

Julian Date	Time (Hrs)	Conc. (dry basis unless noted)			
		NOx (ppmv)	CO (ppmv)	CO2 (%v/v)	O2 (%v/v)
161	11:35:00	21.8	10.5	0.52	19.96
161	11:36:00	12.8	8.9	0.44	20.09
161	11:37:00	17.0	7.5	0.47	20.04
161	11:38:00	20.5	13.6	0.47	20.07
161	11:39:00	13.9	10.3	0.48	20.00
161	11:40:00	16.4	8.0	0.45	20.03
161	11:41:00	22.1	11.9	0.49	20.04
161	11:42:00	12.6	7.9	0.43	20.09
161	11:43:00	15.7	8.9	0.45	20.08
161	11:44:00	24.3	10.6	0.51	19.97
161	11:45:00	13.7	10.7	0.41	20.11
161	11:46:00	14.2	7.1	0.44	20.07
161	11:47:00	22.4	12.1	0.44	20.11
161	11:48:00	16.4	13.1	0.48	19.99
161	11:49:00	14.9	7.4	0.46	20.00
161	11:50:00	22.8	10.9	0.47	20.05
161	11:51:00	16.5	9.6	0.43	20.07
161	11:52:00	13.0	8.4	0.43	20.07
161	11:53:00	16.4	7.2	0.49	19.99
161	11:54:00	22.7	11.3	0.45	20.07
161	11:55:00	15.2	10.2	0.44	20.04
161	11:56:00	14.2	8.0	0.40	20.12
161	11:57:00	24.0	12.2	0.50	19.99
161	11:58:00	18.3	10.2	0.47	20.00
161	11:59:00	13.6	8.2	0.42	20.10
161	12:00:00	18.6	8.1	0.42	20.10
161	12:01:00	21.8	14.7	0.44	20.07
Run Average		16.8	9.7	0.47	20.05

Interpoll Laboratories, Inc.
(612) 786-6020

Printout of ESC Model 80 DAS
for CEM Trailer No. 1
- 1994 -

File Name: LP16
Job Number: 4-3097
Client: Louisiana Pacific Corporation
Location: Hayward, Wisconsin

Line 1 Press RTO Outlet Stack -- Run 3

Julian Date	Time (Hrs)	Conc. (dry basis unless noted)			
		NOx (ppmv)	CO (ppmv)	CO2 (%v/v)	O2 (%v/v)
161	12:21:00	11.3	9.7	0.43	20.40
161	12:22:00	12.1	7.9	0.47	20.36
161	12:23:00	19.1	11.3	0.44	20.42
161	12:24:00	13.1	13.7	0.47	20.37
161	12:25:00	12.2	7.6	0.47	20.34
161	12:26:00	19.6	11.2	0.44	20.45
161	12:27:00	13.4	9.0	0.43	20.42
161	12:28:00	10.3	9.0	0.42	20.46
161	12:29:00	18.9	11.2	0.48	20.37
161	12:30:00	17.3	11.2	0.43	20.41
161	12:31:00	10.8	8.5	0.45	20.42
161	12:32:00	15.0	9.2	0.41	20.48
161	12:33:00	18.3	13.7	0.47	20.40
161	12:34:00	12.0	8.1	0.47	20.35
161	12:35:00	14.9	9.0	0.42	20.45
161	12:36:00	17.8	9.1	0.45	20.39
161	12:37:00	10.5	9.1	0.42	20.45
161	12:38:00	15.3	9.0	0.47	20.34
161	12:39:00	19.3	10.5	0.44	20.39
161	12:40:00	11.4	9.6	0.44	20.41
161	12:41:00	12.1	7.3	0.40	20.47
161	12:42:00	20.6	12.7	0.47	20.40
161	12:43:00	13.0	9.2	0.47	20.35
161	12:44:00	12.9	7.7	0.43	20.41
161	12:45:00	20.8	8.5	0.48	20.34
161	12:46:00	13.1	10.7	0.44	20.43
161	12:47:00	11.8	7.5	0.45	20.35
161	12:48:00	10.5	5.5	0.41	20.41
161	12:49:00	10.3	5.4	0.42	20.44
161	12:50:00	8.5	4.6	0.38	20.50
161	12:51:00	9.8	5.2	0.41	20.46
161	12:52:00	12.1	5.3	0.46	20.35
161	12:53:00	18.1	9.5	0.41	20.45
161	12:54:00	16.2	9.2	0.44	20.40

Interpoll Laboratories, Inc.
(612) 786-6020

Printout of ESC Model 80 DAS
for CEM Trailer No. 1
- 1994 -

File Name: LP16
Job Number: 4-3097
Client: Louisiana Pacific Corporation
Location: Hayward, Wisconsin

Line 1 Press RTO Outlet Stack -- Run 3

Julian Date	Time (Hrs)	Conc. (dry basis unless noted)			
		NOx (ppmv)	CO (ppmv)	CO2 (%v/v)	O2 (%v/v)
161	12:55:00	10.7	7.2	0.40	20.48
161	12:56:00	12.1	6.7	0.46	20.34
161	12:57:00	18.4	8.3	0.43	20.37
161	12:58:00	17.0	11.4	0.43	20.42
161	12:59:00	10.6	6.4	0.38	20.47
161	13:00:00	16.9	9.7	0.42	20.44
161	13:01:00	20.3	10.8	0.48	20.32
161	13:02:00	11.1	8.1	0.38	20.47
161	13:03:00	14.9	6.6	0.42	20.42
161	13:04:00	18.2	11.7	0.41	20.47
161	13:05:00	12.8	8.9	0.45	20.35
161	13:06:00	15.3	6.9	0.43	20.37
161	13:07:00	19.7	10.7	0.43	20.41
161	13:08:00	11.5	6.6	0.37	20.47
161	13:09:00	11.2	6.7	0.40	20.45
161	13:10:00	15.6	6.6	0.46	20.34
161	13:11:00	20.4	11.0	0.41	20.43
161	13:12:00	12.4	8.1	0.41	20.40
161	13:13:00	13.3	7.2	0.39	20.48
161	13:14:00	23.3	12.3	0.48	20.33
161	13:15:00	14.3	8.9	0.43	20.36
161	13:16:00	11.3	6.6	0.40	20.43
161	13:17:00	14.5	6.4	0.39	20.44
161	13:18:00	21.3	12.8	0.43	20.41
161	13:19:00	14.8	9.1	0.45	20.34
161	13:20:00	11.7	5.9	0.38	20.46
161	13:21:00	11.7	4.9	0.41	20.41
Run Average		14.5	8.7	0.43	20.41

Interpoll Laboratories, Inc.
(612) 786-6020

Printout of ESC Model 80 DAS
for CEM Trailer No. 1
- 1994 -

File Name: LPH141
Job Number: 4-3097
Client: Louisiana Pacific Corporation
Location: Hayward, Wisconsin

Line 2 Press RTO Outlet Stack -- Run 1

Julian Date	Time (Hrs)	Conc. (dry basis unless noted)			
		NOx (ppmv)	CO (ppmv)	CO2 (%v/v)	O2 (%v/v)
160	12:41:00	12.0	10.5	0.42	20.45
160	12:42:00	9.9	6.0	0.39	20.48
160	12:43:00	14.9	8.4	0.44	20.42
160	12:44:00	15.4	11.7	0.42	20.45
160	12:45:00	9.4	6.5	0.39	20.44
160	12:46:00	12.1	6.4	0.41	20.47
160	12:47:00	18.0	11.2	0.42	20.45
160	12:48:00	10.6	8.0	0.41	20.44
160	12:49:00	11.2	6.2	0.40	20.46
160	12:50:00	18.2	10.4	0.43	20.44
160	12:51:00	12.3	8.3	0.42	20.42
160	12:52:00	10.2	6.2	0.37	20.48
160	12:53:00	16.2	9.7	0.37	20.53
160	12:54:00	13.0	9.2	0.39	20.47
160	12:55:00	10.2	6.3	0.36	20.52
160	12:56:00	14.7	8.4	0.41	20.44
160	12:57:00	16.1	12.3	0.39	20.46
160	12:58:00	10.5	6.6	0.40	20.44
160	12:59:00	12.2	6.5	0.38	20.46
160	13:00:00	18.6	12.5	0.38	20.49
160	13:01:00	11.4	9.5	0.39	20.46
160	13:02:00	11.5	6.7	0.36	20.50
160	13:03:00	19.4	10.3	0.41	20.43
160	13:04:00	12.6	13.6	0.37	20.47
160	13:05:00	10.7	6.7	0.39	20.45
160	13:06:00	15.2	9.0	0.39	20.47
160	13:07:00	16.6	12.2	0.39	20.45
160	13:08:00	10.0	9.1	0.36	20.48
160	13:09:00	14.4	7.9	0.40	20.43
160	13:10:00	18.9	12.6	0.40	20.45
160	13:11:00	10.4	9.2	0.36	20.46
160	13:12:00	11.9	7.8	0.36	20.52
160	13:13:00	20.4	9.9	0.42	20.40
160	13:14:00	12.5	11.3	0.36	20.47

Interpoll Laboratories, Inc.
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Printout of ESC Model 80 DAS
for CEM Trailer No. 1
- 1994 -

File Name: LPH141
Job Number: 4-3097
Client: Louisiana Pacific Corporation
Location: Hayward, Wisconsin

Line 2 Press RTO Outlet Stack -- Run 1

Julian Date	Time (Hrs)	Conc. (dry basis unless noted)			
		NOx (ppmv)	CO (ppmv)	CO2 (%v/v)	O2 (%v/v)
160	13:15:00	11.4	6.9	0.38	20.44
160	13:16:00	18.9	11.5	0.37	20.48
160	13:17:00	14.6	9.4	0.41	20.39
160	13:18:00	11.6	7.0	0.38	20.41
160	13:19:00	16.4	8.9	0.39	20.45
160	13:20:00	16.3	14.1	0.36	20.47
160	13:21:00	11.0	7.9	0.37	20.46
160	13:22:00	16.3	9.0	0.40	20.42
160	13:23:00	19.0	11.4	0.39	20.42
160	13:24:00	10.9	8.9	0.35	20.47
160	13:25:00	13.9	6.9	0.36	20.47
160	13:26:00	22.0	10.8	0.42	20.38
160	13:27:00	12.3	9.3	0.36	20.45
160	13:28:00	11.9	7.0	0.34	20.48
160	13:29:00	20.1	10.1	0.37	20.47
160	13:30:00	14.5	8.1	0.39	20.42
160	13:31:00	12.2	6.8	0.36	20.45
160	13:32:00	17.7	8.7	0.37	20.44
160	13:33:00	16.8	13.0	0.37	20.45
160	13:34:00	12.3	9.9	0.38	20.40
160	13:35:00	16.8	8.2	0.37	20.44
160	13:36:00	18.9	9.7	0.39	20.40
160	13:37:00	11.0	8.4	0.32	20.50
160	13:38:00	12.9	5.8	0.38	20.42
160	13:39:00	20.7	9.9	0.39	20.40
160	13:40:00	13.9	9.7	0.36	20.44
160	13:41:00	10.6	6.9	0.32	20.49
160	13:42:00	16.6	7.7	0.38	20.43
Run Average		14.2	9.0	0.38	20.45

Interpoll Laboratories, Inc.
(612) 786-6020

Printout of ESC Model 80 DAS
for CEM Trailer No. 1
- 1994 -

File Name: LPH142
Job Number: 4-3097
Client: Louisiana Pacific Corporation
Location: Hayward, Wisconsin

Line 2 Press RTO Outlet Stack -- Run 2

Julian Date	Time (Hrs)	Conc. (dry basis unless noted)			
		NOx (ppmv)	CO (ppmv)	CO2 (%v/v)	O2 (%v/v)
160	14:26:00	8.0	12.2	0.35	20.45
160	14:27:00	9.5	10.8	0.35	20.49
160	14:28:00	16.8	14.1	0.38	20.43
160	14:29:00	9.1	14.1	0.35	20.46
160	14:30:00	8.2	10.3	0.34	20.48
160	14:31:00	16.3	13.9	0.39	20.43
160	14:32:00	10.3	15.4	0.36	20.44
160	14:33:00	7.5	10.4	0.34	20.47
160	14:34:00	13.0	12.7	0.36	20.44
160	14:35:00	13.6	15.1	0.38	20.43
160	14:36:00	7.4	11.1	0.34	20.47
160	14:37:00	12.0	12.0	0.34	20.47
160	14:38:00	15.3	16.2	0.39	20.40
160	14:39:00	7.9	12.1	0.35	20.45
160	14:40:00	10.9	10.6	0.35	20.45
160	14:41:00	16.1	15.7	0.38	20.40
160	14:42:00	8.7	13.5	0.35	20.45
160	14:43:00	9.4	9.6	0.35	20.47
160	14:44:00	16.1	14.2	0.36	20.42
160	14:45:00	10.3	14.5	0.36	20.43
160	14:46:00	8.5	9.7	0.34	20.45
160	14:47:00	13.9	13.2	0.35	20.46
160	14:48:00	12.9	13.6	0.37	20.41
160	14:49:00	8.3	10.2	0.35	20.43
160	14:50:00	11.9	12.0	0.36	20.45
160	14:51:00	14.9	14.5	0.37	20.40
160	14:52:00	8.3	11.2	0.33	20.45
160	14:53:00	10.7	11.0	0.33	20.47
160	14:54:00	15.5	15.2	0.37	20.44
160	14:55:00	8.8	12.1	0.34	20.46
160	14:56:00	9.6	9.8	0.34	20.45
160	14:57:00	16.6	14.2	0.37	20.41
160	14:58:00	10.3	14.0	0.36	20.43
160	14:59:00	8.9	9.8	0.33	20.44

Interpoll Laboratories, Inc.
(612) 786-6020

Printout of ESC Model 80 DAS
for CEM Trailer No. 1
- 1994 -

File Name: LPH142
Job Number: 4-3097
Client: Louisiana Pacific Corporation
Location: Hayward, Wisconsin

Line 2 Press RTO Outlet Stack -- Run 2

Julian Date	Time (Hrs)	Conc. (dry basis unless noted)			
		NOx (ppmv)	CO (ppmv)	CO2 (%v/v)	O2 (%v/v)
160	15:00:00	15.8	12.9	0.35	20.44
160	15:01:00	12.0	14.8	0.36	20.41
160	15:02:00	8.7	9.9	0.33	20.46
160	15:03:00	13.4	11.8	0.34	20.47
160	15:04:00	15.1	16.0	0.36	20.40
160	15:05:00	8.8	11.0	0.34	20.45
160	15:06:00	12.0	10.3	0.34	20.46
160	15:07:00	16.4	16.2	0.34	20.42
160	15:08:00	9.8	12.7	0.34	20.43
160	15:09:00	10.6	9.7	0.34	20.45
160	15:10:00	17.2	14.8	0.35	20.43
160	15:11:00	11.3	13.4	0.35	20.40
160	15:12:00	9.6	9.5	0.33	20.44
160	15:13:00	15.9	13.4	0.35	20.46
160	15:14:00	13.1	14.1	0.34	20.42
160	15:15:00	9.5	10.1	0.33	20.44
160	15:16:00	13.8	12.5	0.34	20.45
160	15:17:00	15.8	15.5	0.36	20.41
160	15:18:00	9.6	10.4	0.33	20.45
160	15:19:00	12.5	11.1	0.33	20.46
160	15:20:00	16.5	16.1	0.34	20.41
160	15:21:00	10.0	11.3	0.34	20.43
160	15:22:00	10.9	9.7	0.32	20.45
160	15:23:00	17.5	14.2	0.35	20.44
160	15:24:00	10.9	14.1	0.35	20.40
160	15:25:00	9.6	9.4	0.33	20.45
160	15:26:00	16.2	12.1	0.34	20.45
160	15:27:00	13.3	14.9	0.34	20.40
Run Average		12.0	12.6	0.35	20.44

Interpoll Laboratories, Inc.
(612) 786-6020

Printout of ESC Model 80 DAS
for CEM Trailer No. 1
- 1994 -

File Name: LPH143
Job Number: 4-3097
Client: Louisiana Pacific Corporation
Location: Hayward, Wisconsin

Line 2 Press RTO Outlet Stack -- Run 3

Julian Date	Time (Hrs)	Conc. (dry basis unless noted)			
		NOx (ppmv)	CO (ppmv)	CO2 (%v/v)	O2 (%v/v)
160	16:06:00	13.2	15.6	0.35	20.41
160	16:07:00	6.3	10.6	0.36	20.42
160	16:08:00	8.1	9.7	0.34	20.43
160	16:09:00	13.5	14.1	0.36	20.43
160	16:10:00	6.9	12.4	0.36	20.39
160	16:11:00	7.0	8.9	0.34	20.44
160	16:12:00	13.9	12.5	0.36	20.43
160	16:13:00	8.1	13.9	0.34	20.40
160	16:14:00	6.4	8.7	0.35	20.42
160	16:15:00	11.3	10.8	0.36	20.42
160	16:16:00	11.1	15.8	0.34	20.44
160	16:17:00	6.1	9.6	0.35	20.42
160	16:18:00	9.5	10.4	0.34	20.43
160	16:19:00	12.8	16.5	0.35	20.44
160	16:20:00	6.3	10.8	0.34	20.41
160	16:21:00	8.4	9.8	0.34	20.42
160	16:22:00	13.4	15.0	0.35	20.42
160	16:23:00	6.7	11.1	0.34	20.41
160	16:24:00	6.7	8.5	0.33	20.43
160	16:25:00	12.8	13.0	0.35	20.43
160	16:26:00	7.9	13.2	0.32	20.42
160	16:27:00	5.7	9.0	0.34	20.43
160	16:28:00	10.0	11.4	0.34	20.44
160	16:29:00	11.1	15.2	0.34	20.43
160	16:30:00	5.3	9.7	0.34	20.40
160	16:31:00	8.8	10.0	0.34	20.44
160	16:32:00	12.9	15.2	0.35	20.43
160	16:33:00	5.2	10.9	0.32	20.42
160	16:34:00	7.5	9.2	0.34	20.43
160	16:35:00	13.5	13.8	0.36	20.41
160	16:36:00	5.9	12.2	0.31	20.45
160	16:37:00	5.6	8.2	0.33	20.42
160	16:38:00	10.6	11.2	0.34	20.41
160	16:39:00	10.9	16.3	0.34	20.43

Interpoll Laboratories, Inc.
(612) 786-6020

Printout of ESC Model 80 DAS
for CEM Trailer No. 1
- 1994 -

File Name: LPH143
Job Number: 4-3097
Client: Louisiana Pacific Corporation
Location: Hayward, Wisconsin

Line 2 Press RTO Outlet Stack -- Run 3

Julian Date	Time (Hrs)	Conc. (dry basis unless noted)			
		NOx (ppmv)	CO (ppmv)	CO2 (%v/v)	O2 (%v/v)
160	16:40:00	5.6	9.6	0.34	20.40
160	16:41:00	8.9	10.1	0.34	20.41
160	16:42:00	12.4	16.0	0.35	20.42
160	16:43:00	5.6	10.6	0.34	20.42
160	16:44:00	7.3	9.2	0.33	20.43
160	16:45:00	13.1	14.3	0.35	20.42
160	16:46:00	5.9	11.1	0.32	20.42
160	16:47:00	6.6	9.0	0.34	20.43
160	16:48:00	12.8	12.9	0.34	20.42
160	16:49:00	6.9	13.1	0.32	20.43
160	16:50:00	5.0	9.1	0.34	20.41
160	16:51:00	9.5	11.4	0.32	20.45
160	16:52:00	10.5	15.0	0.32	20.45
160	16:53:00	4.7	10.2	0.33	20.39
160	16:54:00	8.1	9.7	0.35	20.42
160	16:55:00	12.7	14.9	0.36	20.41
160	16:56:00	4.7	11.1	0.31	20.41
160	16:57:00	6.9	8.8	0.34	20.41
160	16:58:00	13.2	13.7	0.35	20.40
160	16:59:00	5.1	12.2	0.30	20.45
160	17:00:00	5.7	8.8	0.33	20.41
160	17:01:00	12.3	12.2	0.34	20.40
160	17:02:00	6.8	14.4	0.32	20.43
160	17:03:00	4.5	8.2	0.33	20.41
160	17:04:00	7.9	9.6	0.33	20.42
160	17:05:00	11.0	14.9	0.34	20.42
160	17:06:00	4.7	10.0	0.32	20.42
160	17:07:00	6.2	8.4	0.32	20.43
160	17:08:00	11.7	13.0	0.33	20.43
160	17:09:00	5.1	11.1	0.30	20.43
160	17:10:00	5.4	8.7	0.33	20.42
160	17:11:00	11.8	11.9	0.34	20.42
160	17:12:00	6.1	12.6	0.31	20.44
160	17:13:00	4.3	8.8	0.32	20.41

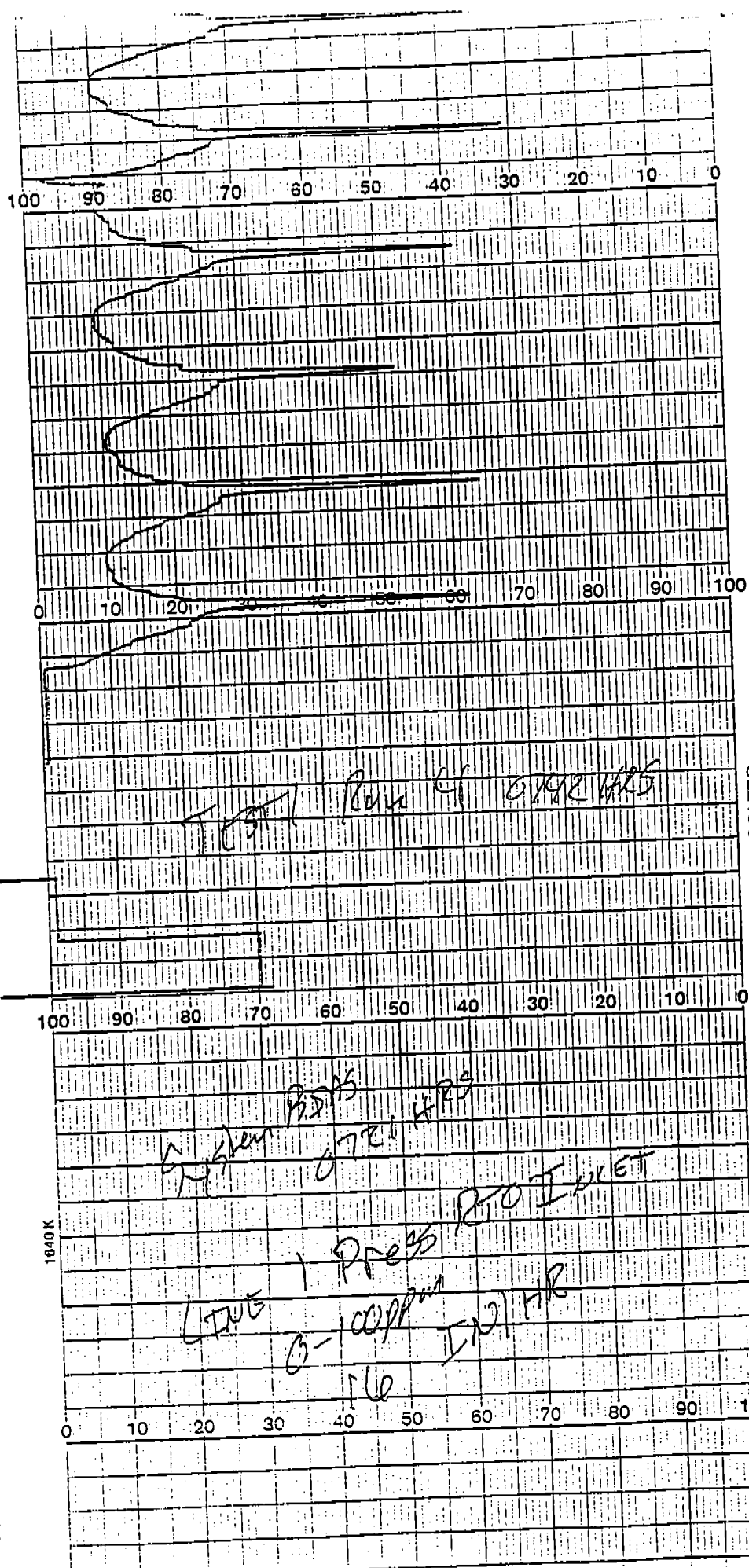
Interpoll Laboratories, Inc.
(612) 786-6020

Printout of ESC Model 80 DAS
for CEM Trailer No. 1
- 1994 -

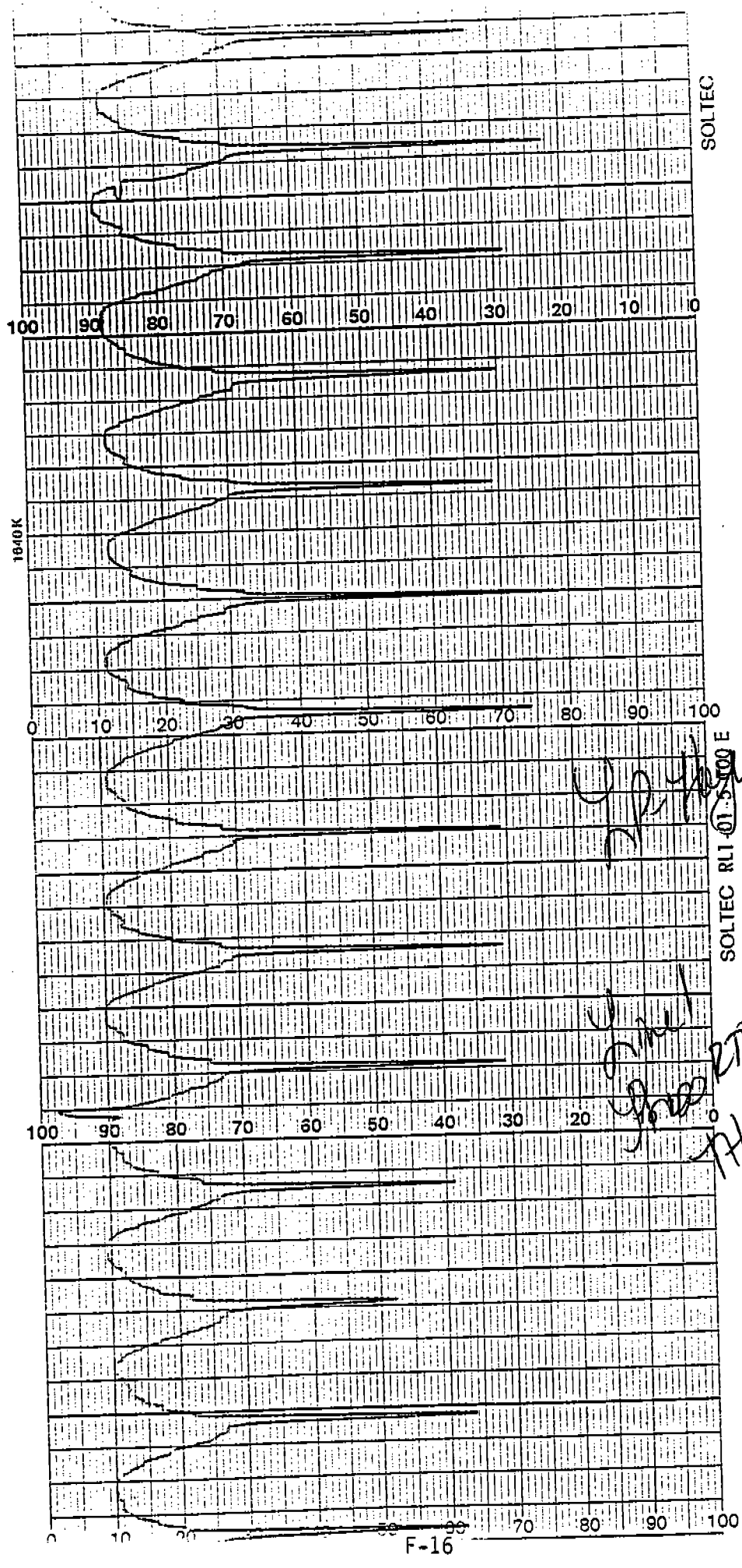
File Name: LPH143
Job Number: 4-3097
Client: Louisiana Pacific Corporation
Location: Hayward, Wisconsin

Line 2 Press RTO Outlet Stack -- Run 3

Julian Date	Time (Hrs)	Conc. (dry basis unless noted)			
		NOx (ppmv)	CO (ppmv)	CO2 (%v/v)	O2 (%v/v)
160	17:14:00	9.2	10.6	0.34	20.43
160	17:15:00	8.4	14.1	0.33	20.43
160	17:16:00	3.7	8.9	0.31	20.42
160	17:17:00	5.7	9.0	0.34	20.28
Run Average		8.4	11.5	0.34	20.42



SOLTEC



SOLTEC

100 90 80 70 60 50 40 30 20 10 0

1840K

0 10 20 30 40 50 60 70 80 90 100

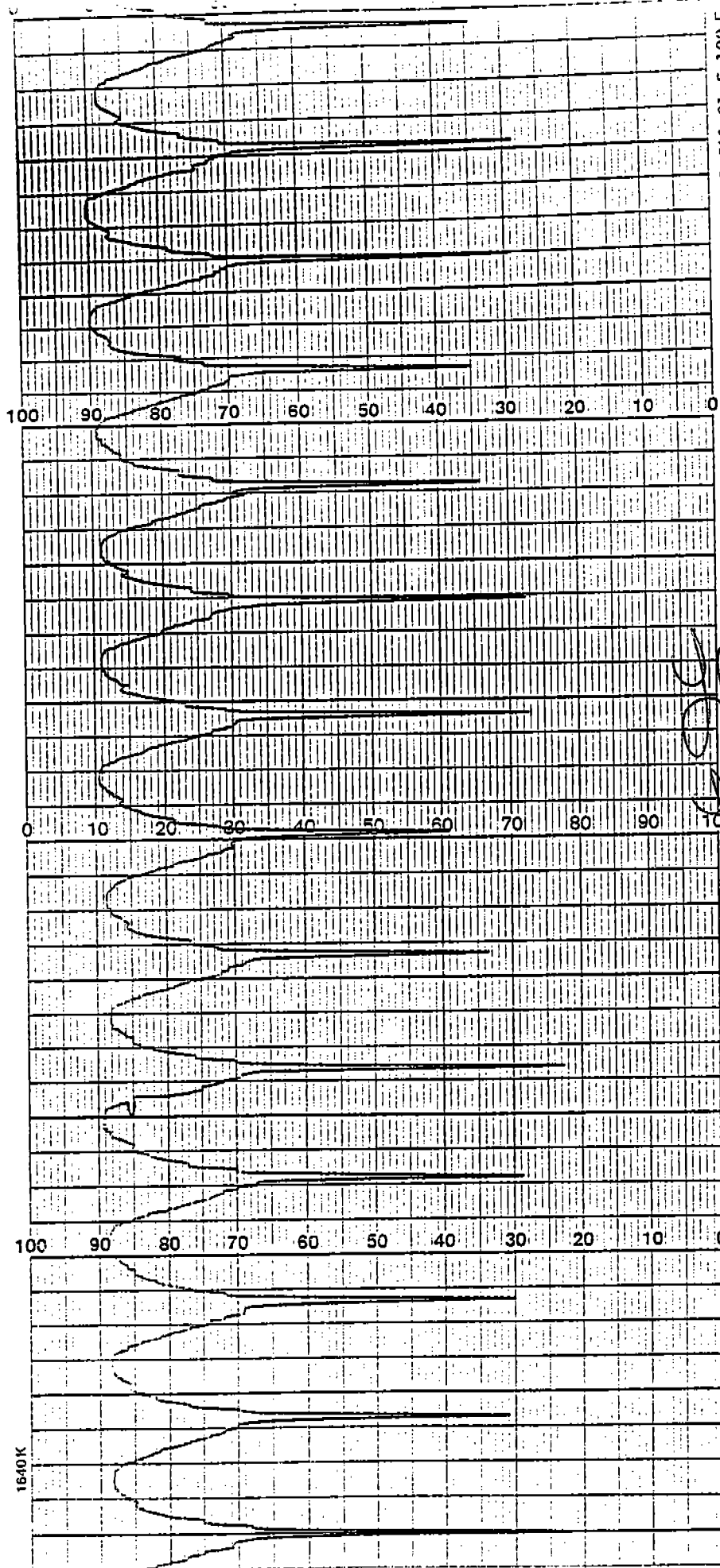
SOLTEC RL1 01-5-500 E

100 90 80 70 60 50 40 30 20 0

F-16

Handwritten signature

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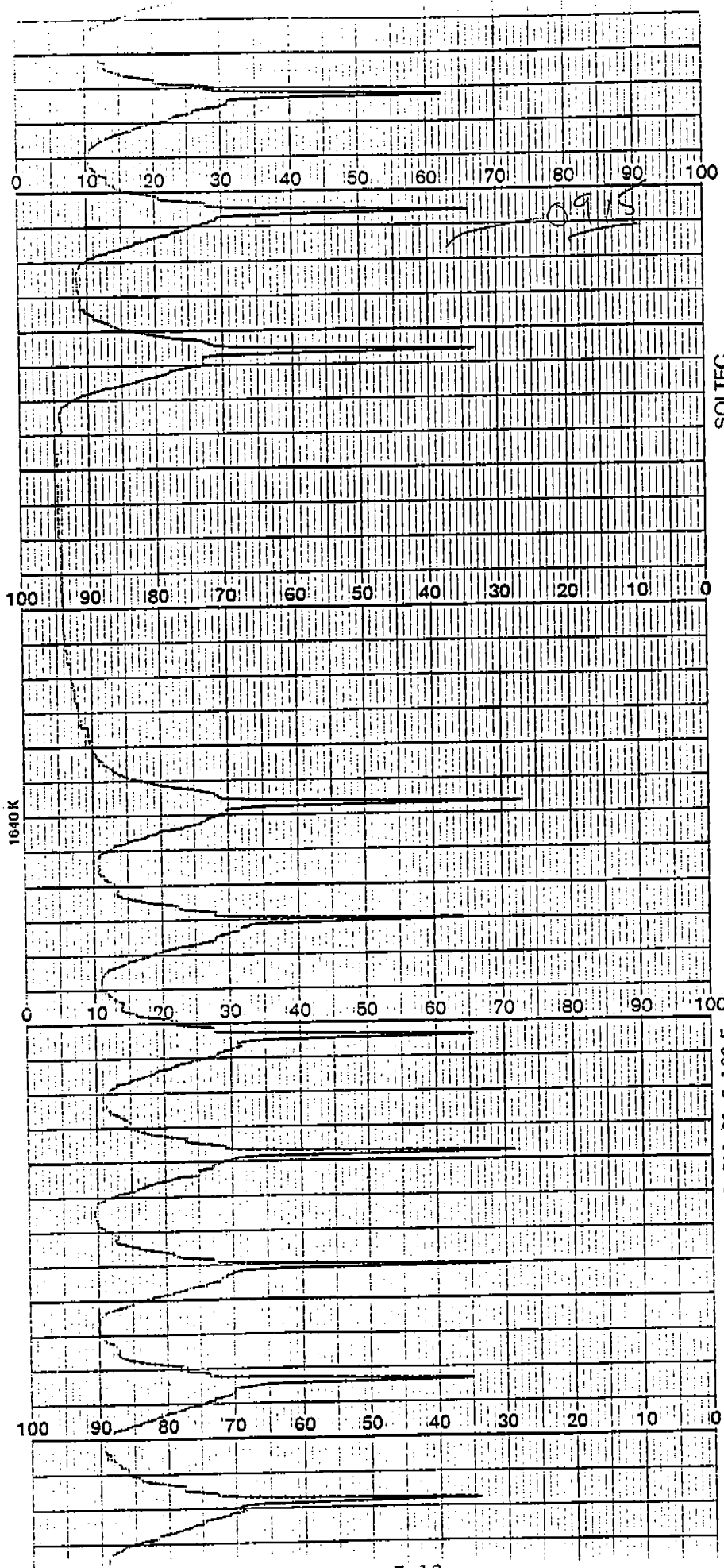


SOLTEC RL1-01-5-100 E

SOLTEC

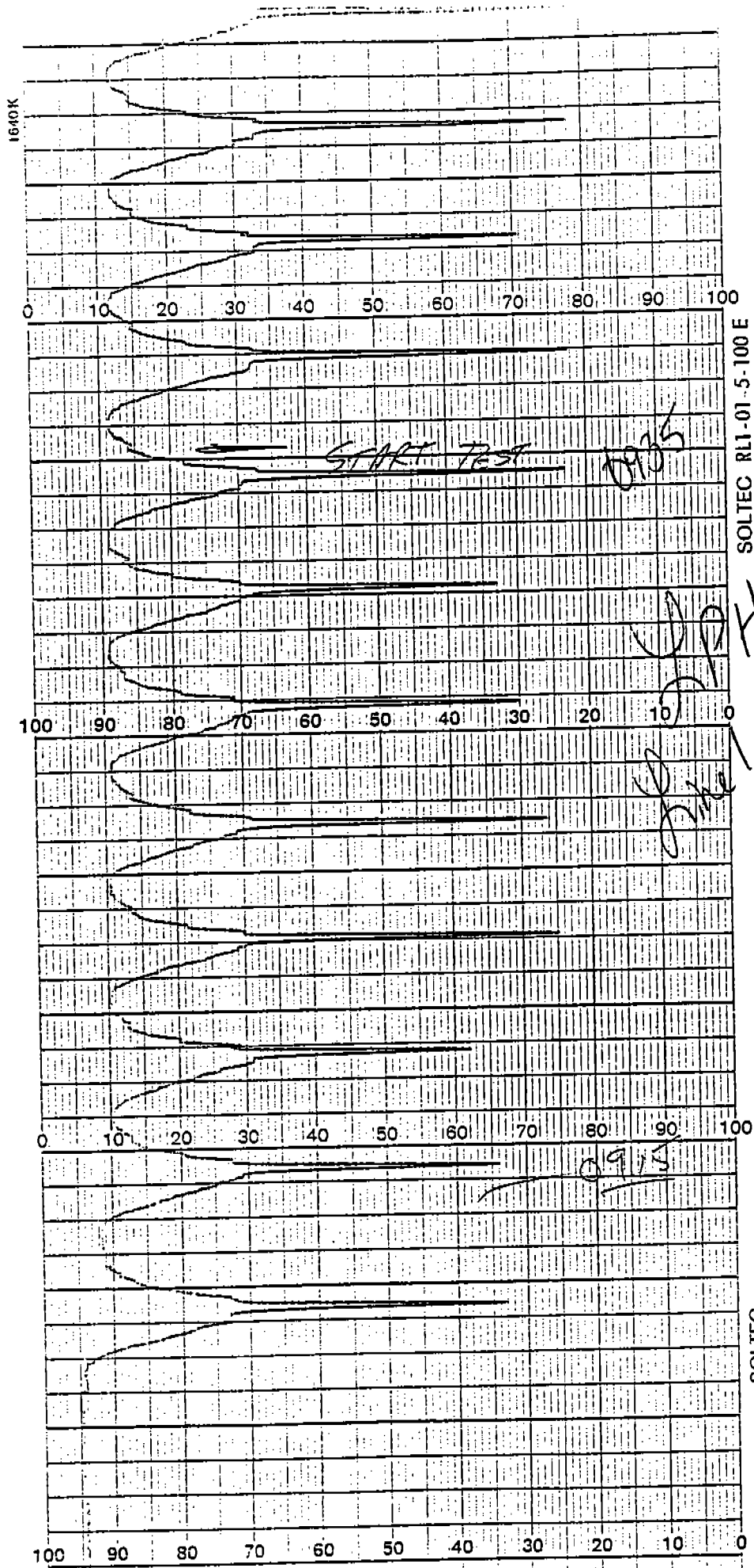
1840K

Handwritten:
P. Hayward
S. M. Press
PTO act



SOLTEC

SOLTEC RL1-01-5-100 E



70K1 - Mang

0 10 20 30 40 50 60 70 80 90 100

SOLTEC

100 90 80 70 60 50 40 30 20 10

1640 K

0 10 20 30 40 50 60 70 80 90 100

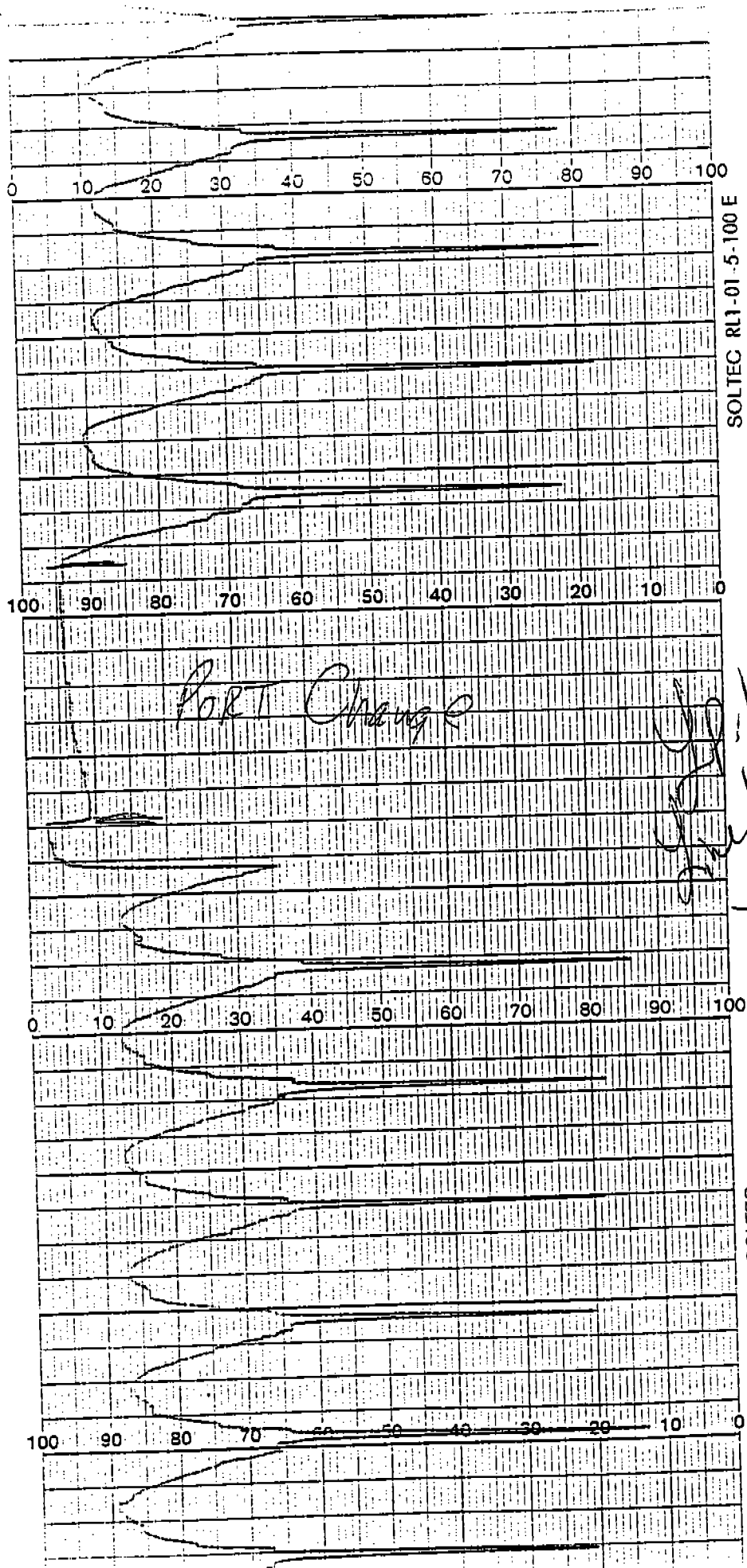
SOLTEC RL1-01-5-100 E

START TEST

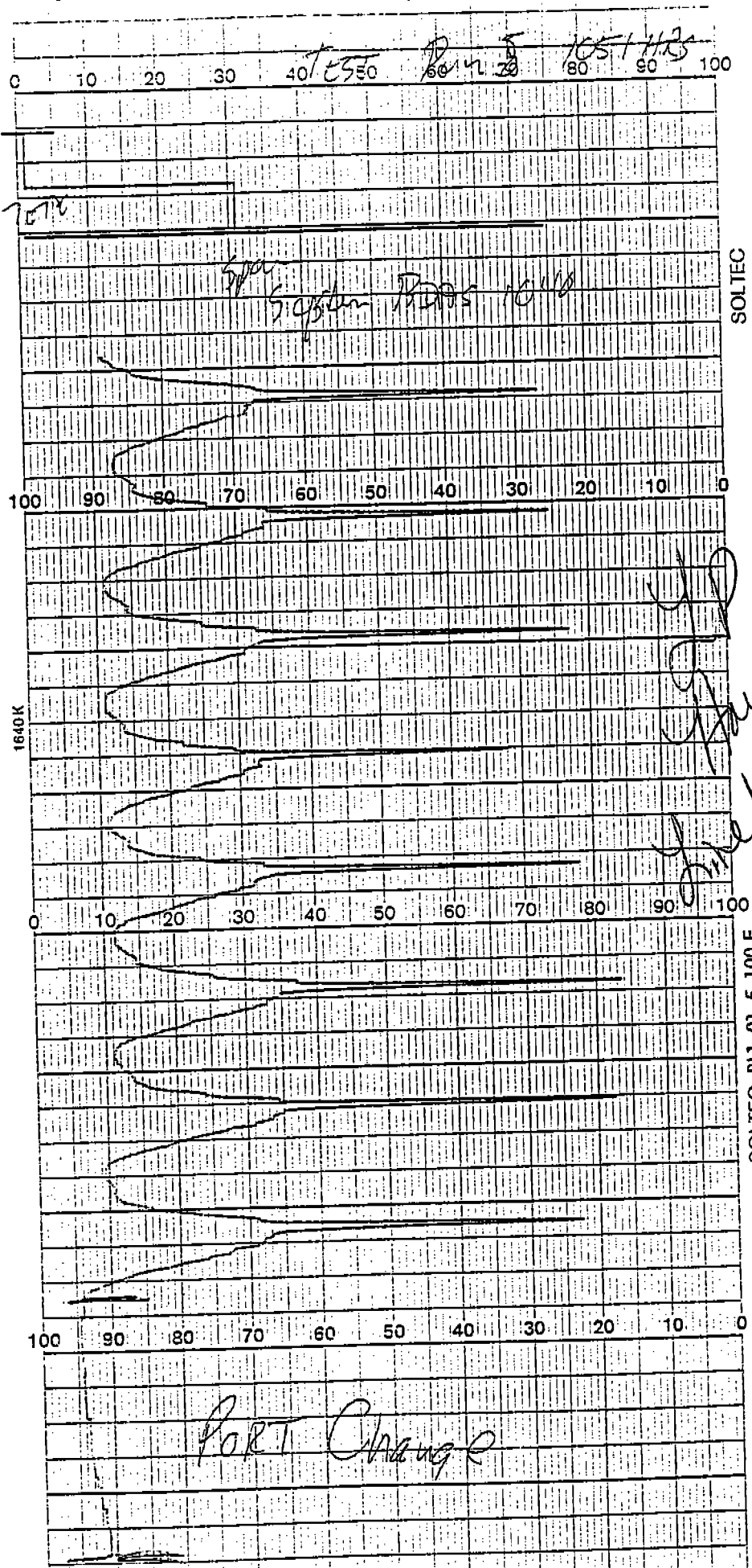
100 90 80 70 60 50 40 30 20 10 0

F-20

AP Haywood
Intel Product

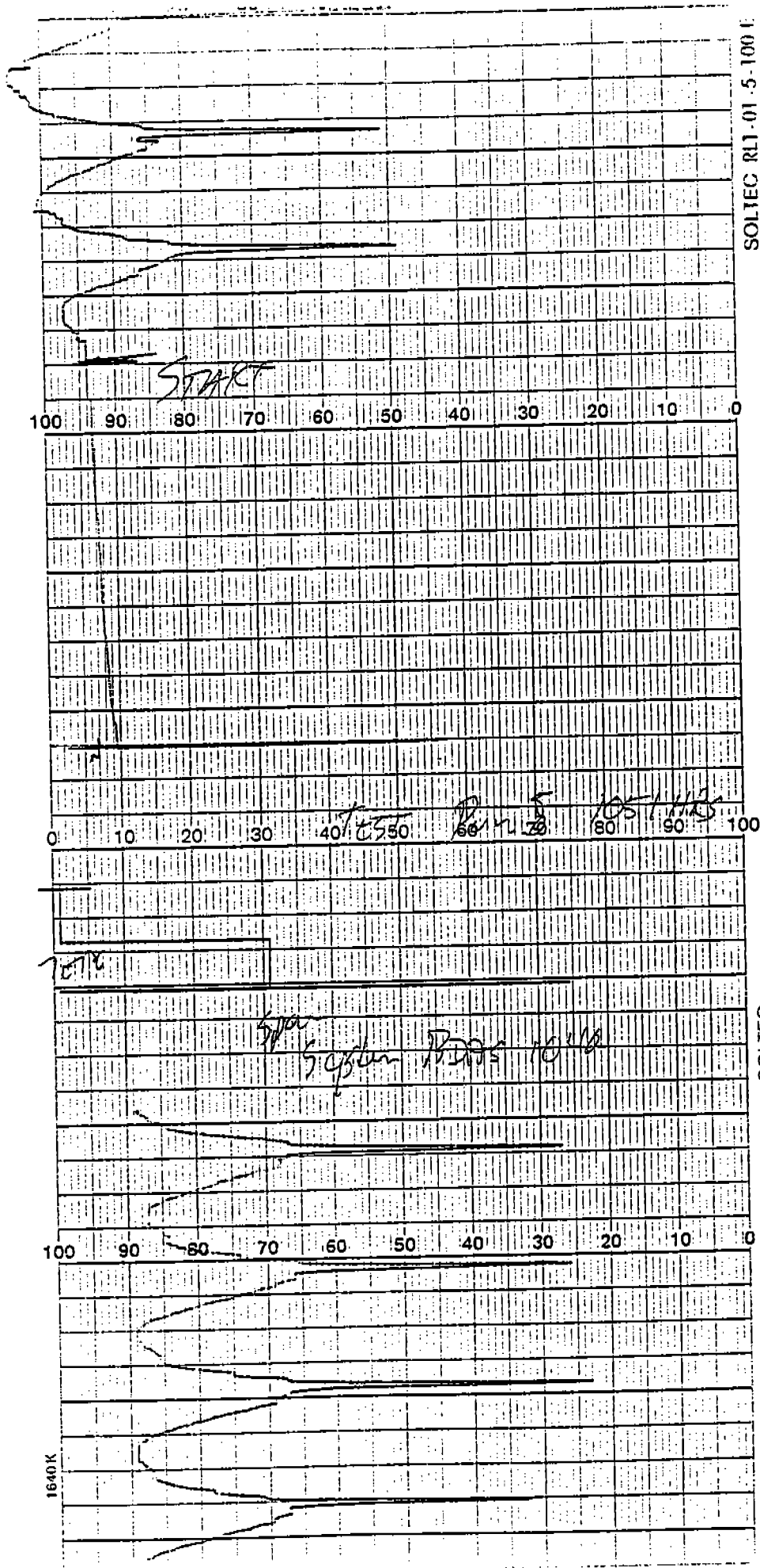


Hybrid
1270
Alert



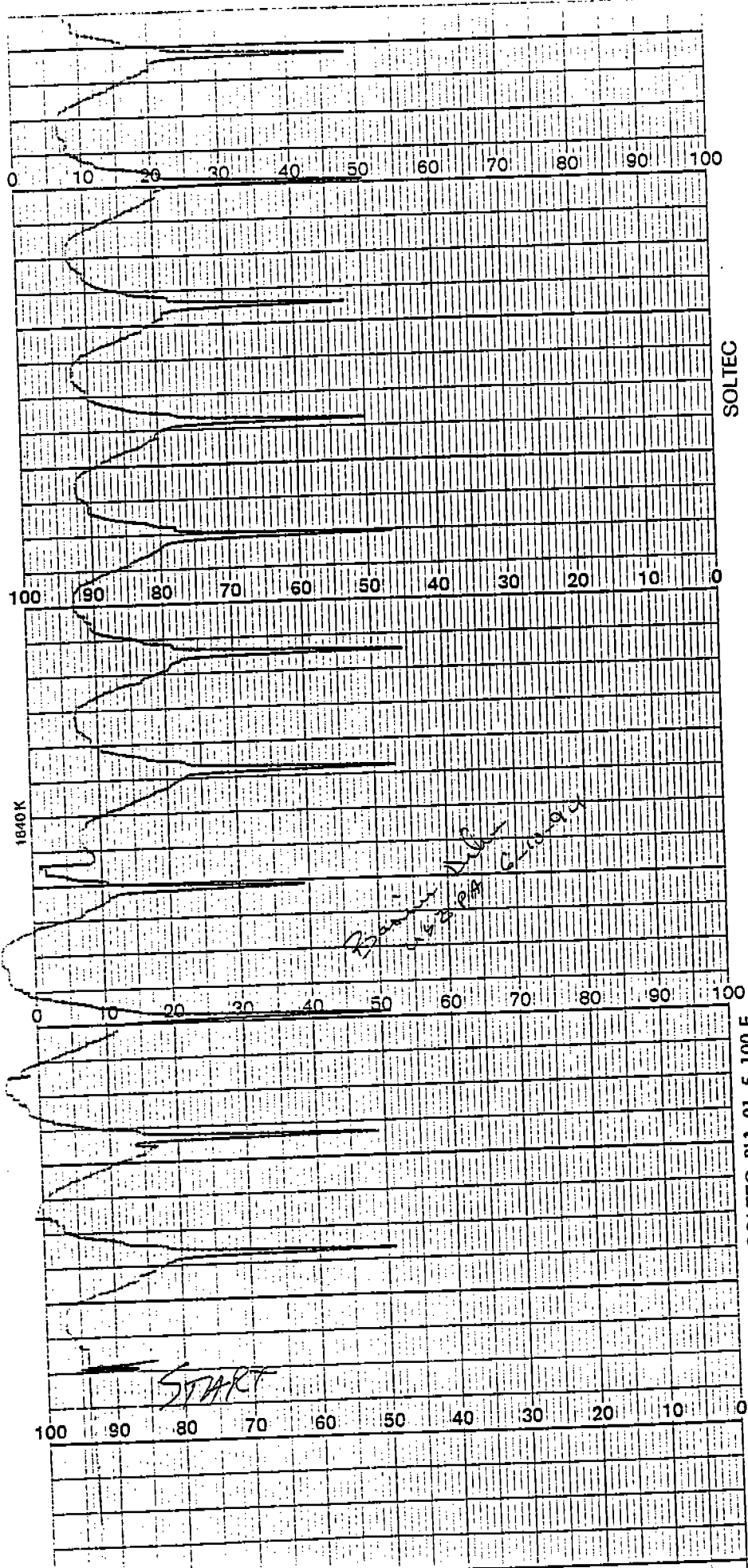
PORT Change

Handwritten notes and signatures on the right side of the page, including "Hayward" and "Kralet".



SOLTEC RL1-01 5-100 E

SOLTEC



SOLTEC

100 90 80 70 60 50 40 30 20 10 0

FAST Run 56/1218 HRS

1640K

FAST Run 1200 HRS

0 10 20 30 40 50 60 70 80 90 100

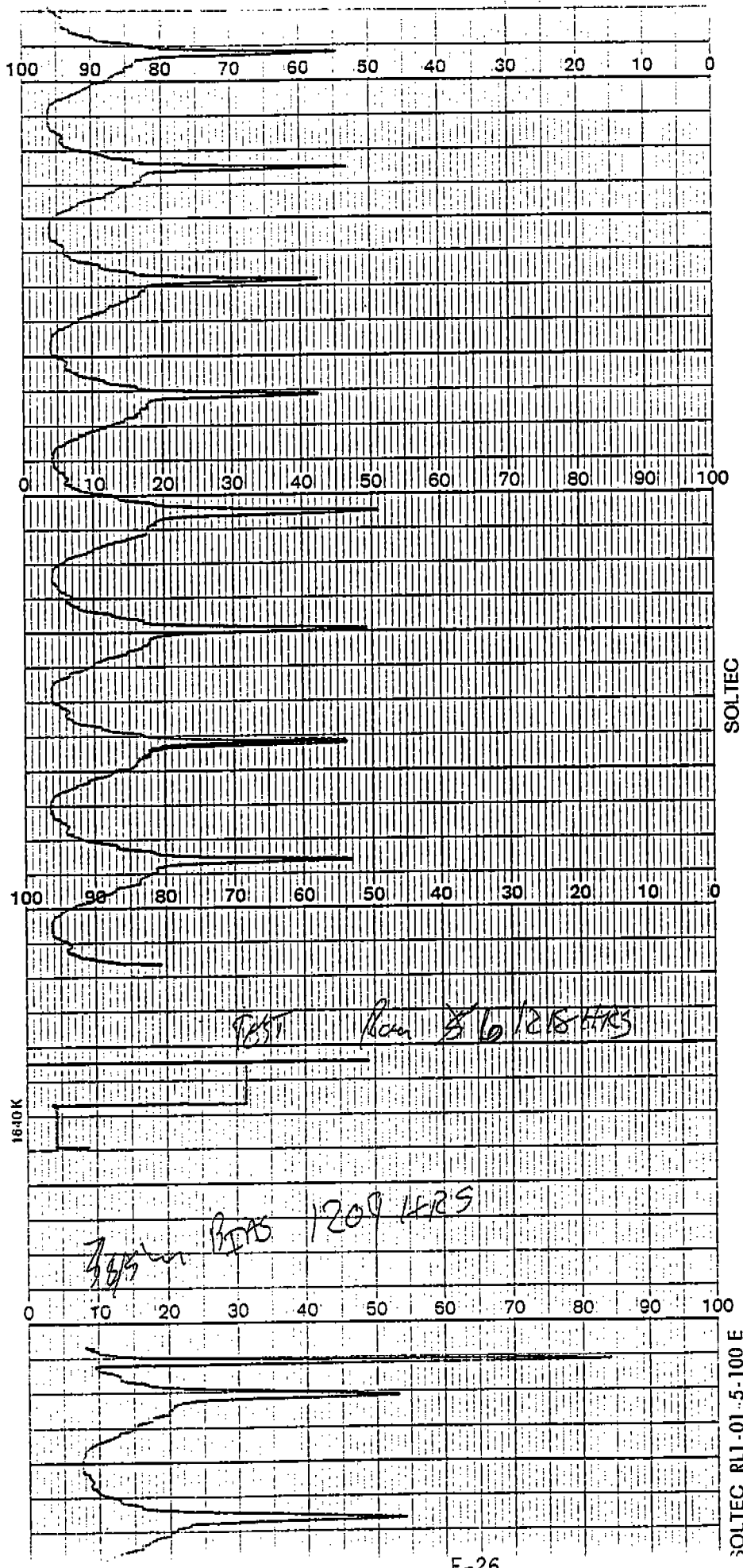
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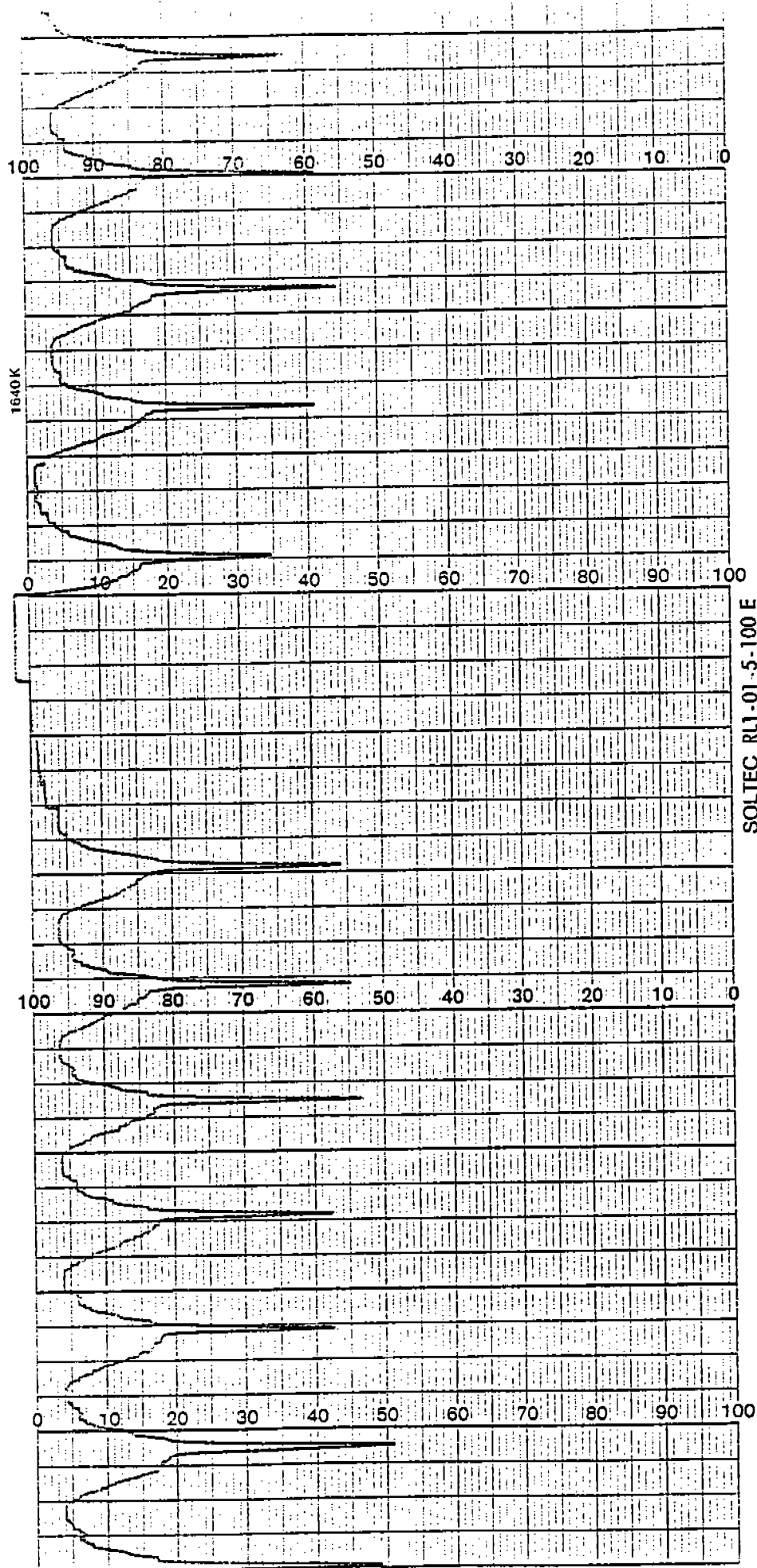
Chart 2000
STICK

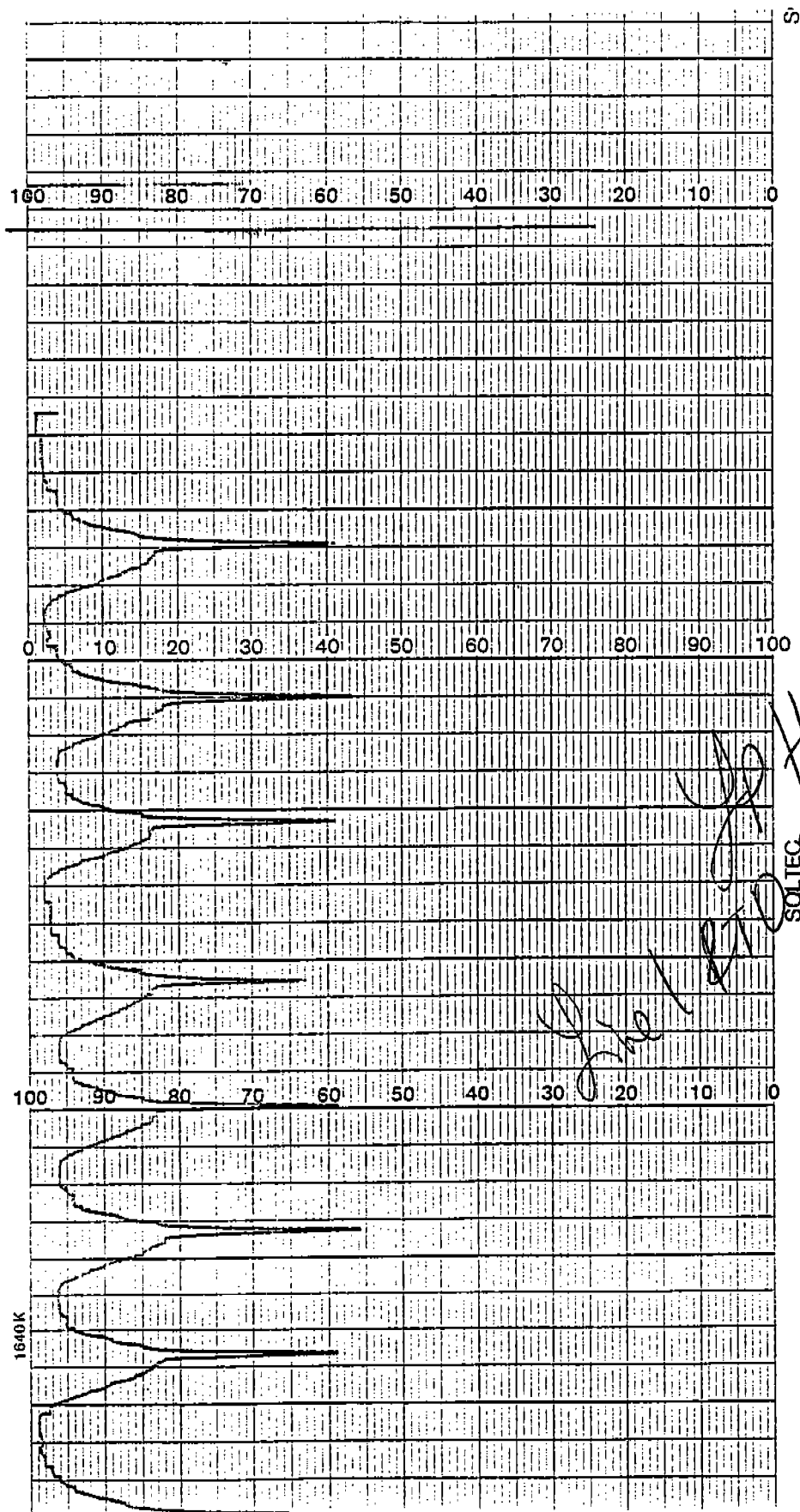
0 10 20 30 40 50 60 70 80 90 100

SOLTEC



SOLTEC





10 20 30 40 50 60 70 80 90 100

TEST 1 Room 4 CTR HP
(Room 1)

J.P. Hayward

LINE 1 PRESS RTG STACK

0-100ppm

16 IN / HR

THCS AS Carbon

100 90 80 70 60 50 40 30 20 10 0

Handwritten notes on the left margin, including "Handwritten" and "Handwritten" repeated vertically.

Lowered - 600
0915

0 10 20 30 40 50 60 70 80 90 100

90 80 70 60 50 40 30 20 10 0

NO. INR 0100-0017

U.S. CORPORATION BUFFALO, NEW YORK

Handwritten notes along the left margin, including "11" at the bottom.

0 10 20 30 40 50 60 70 80 90 100

—

START TEST

90 80 70 60 50 40 30 20 10 0

Lowered TEC
0945

Up Haywood
Line 1-270
Stack

PRINTED IN U.S.A.

TEST 1 Run 5 1051 HRS

NO. IN

Span

7020

Signal Base 1047

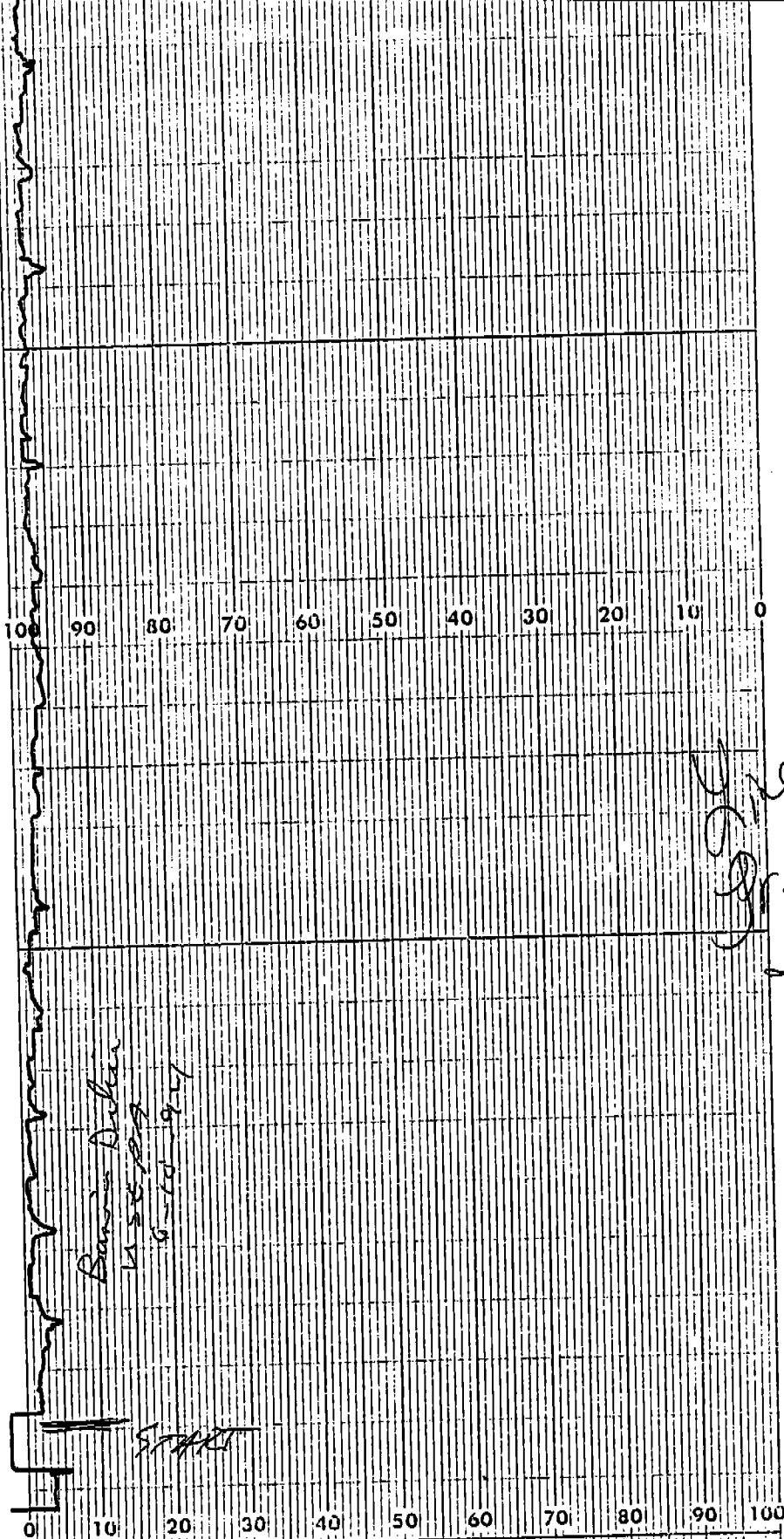
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Handwritten notes: Hayward, 700 PTO, Stack

100 90 80 70 60 50 40 30 20 10 0

0 10 20 30 40 50 60 70 80 90 100

GRAPHIC CONTROLS CORPORATION BUFFALO, NEW YORK



PRINTED IN U.S.A.

NO. 1NR 6109-0317

FEST 1 Row 5 1051 HRS

7026

Superior Bros 1007

12th April 12th APR 65

100 90 80 70 60 50 40 30 20 10 0



100

12th April 12th APR 65



0 10 20 30 40 50 60 70 80 90 100

UP Hayward
12th April 12th APR 65
Stack

GRAPHIC CONTROLS CORPORATION BUFFALO, NEW YORK

PRINTED IN U.S.A.

0 10 20 30 40 50 60 70 80 90 100

NO. INC 0100-0017

100 90 80 70 60 50 40 30 20 10 0

TEST Run C 12/18/75

100

System BINS 1207

GRAPHIC CONTROLS CORPORATION BUFFALO, NEW YORK

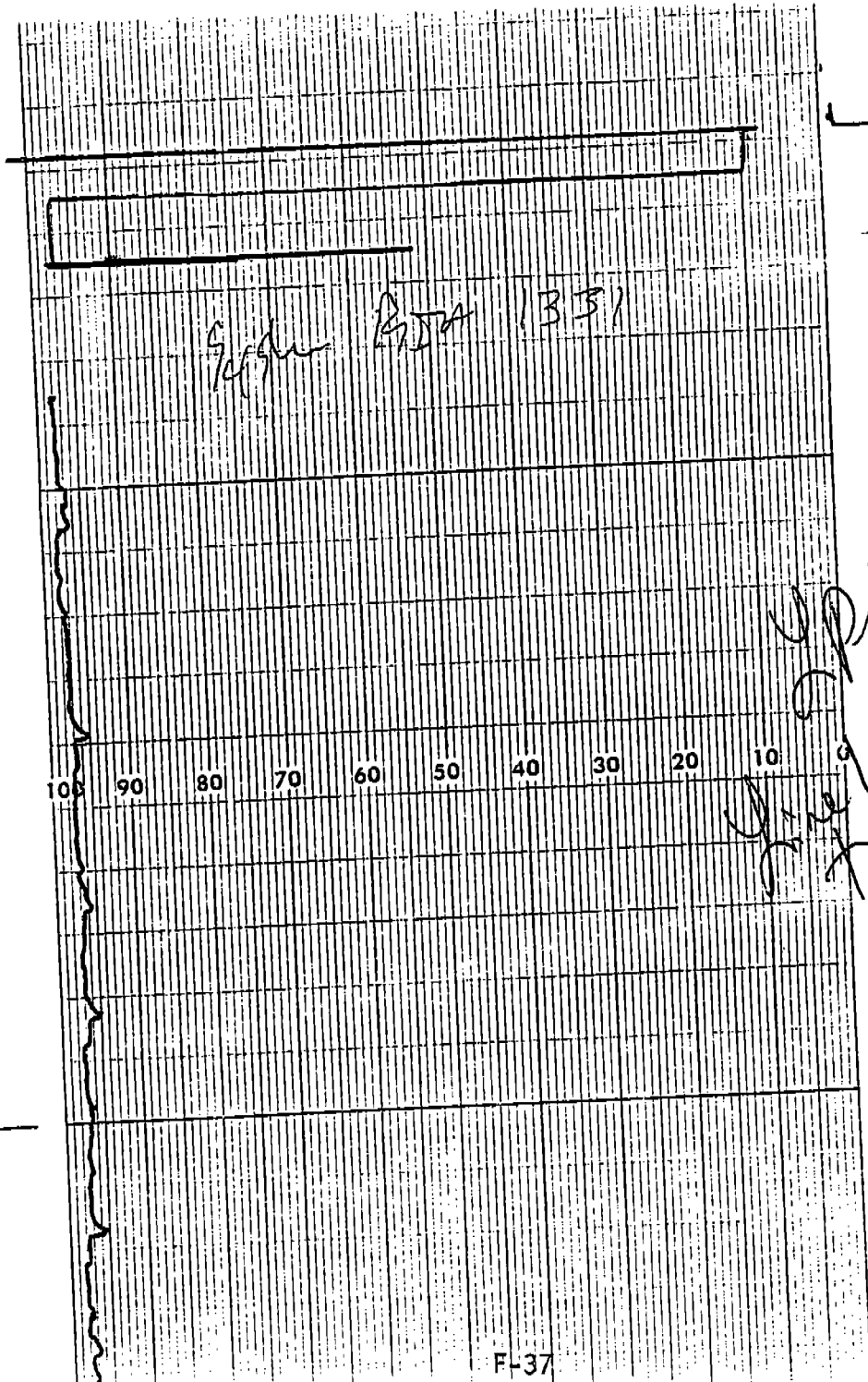
Spd EJA 1331

PRINTED IN U.S.A.

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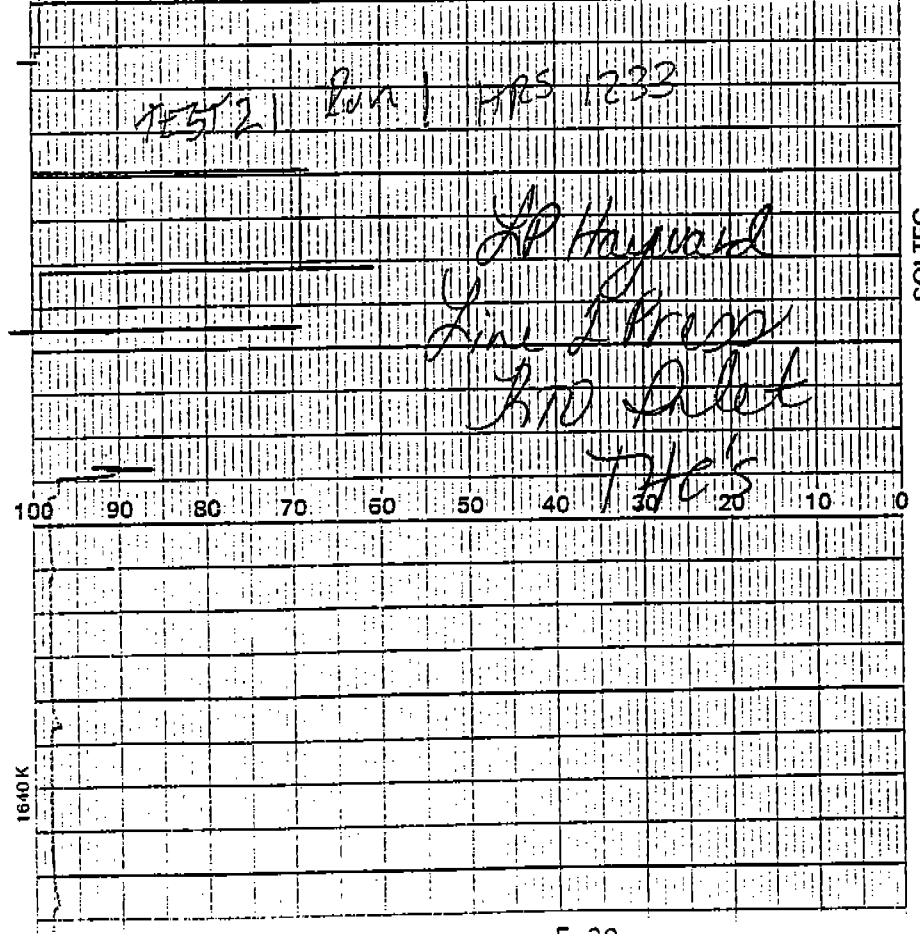
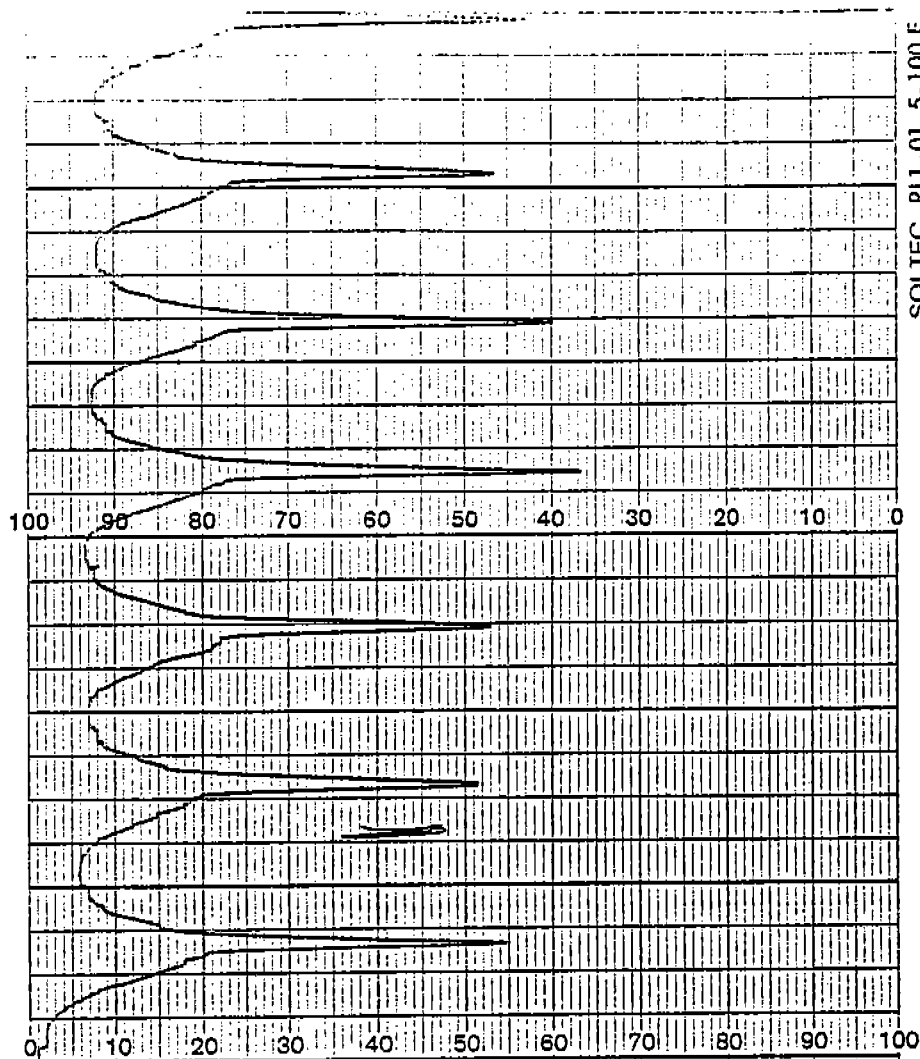
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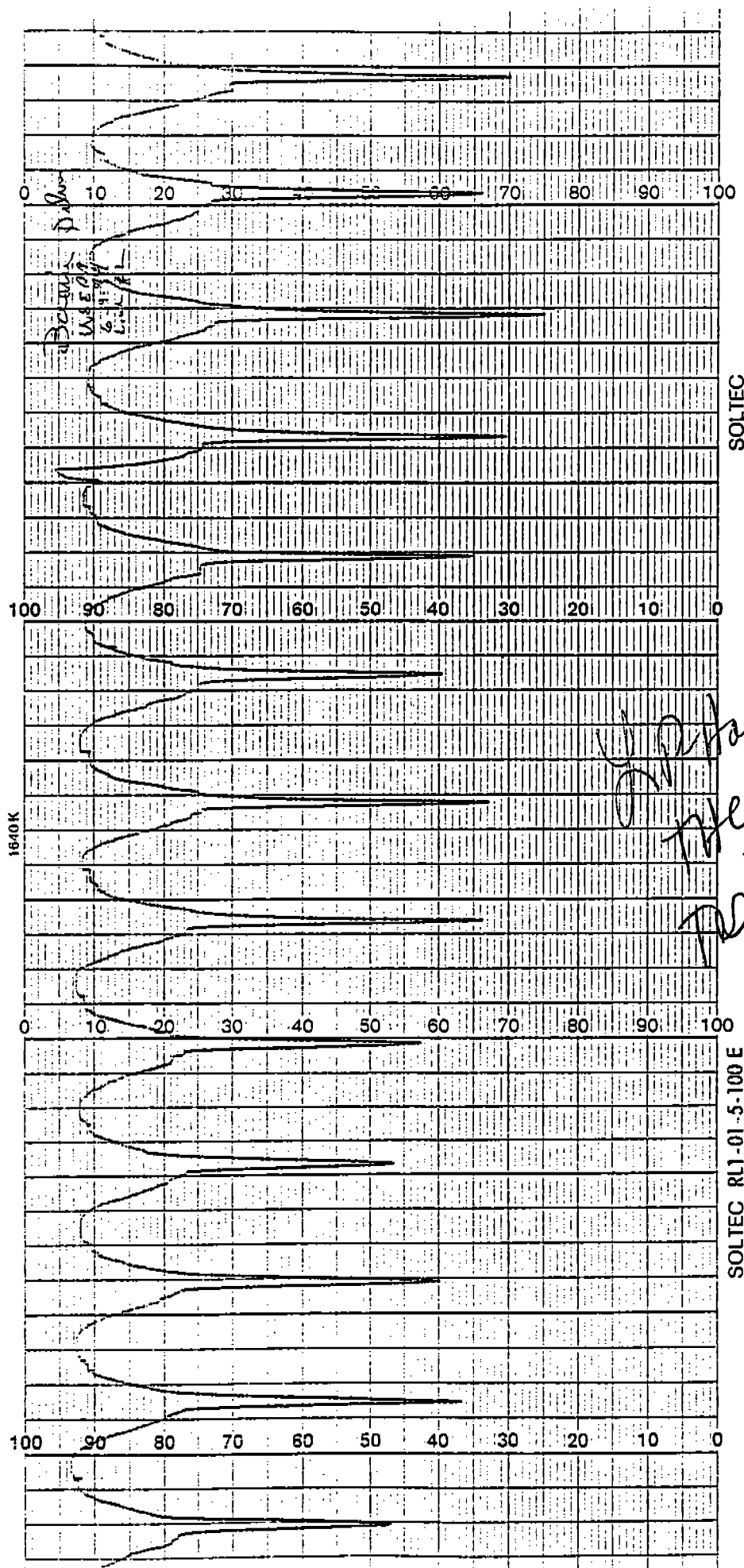
NO. INC 0100-0017



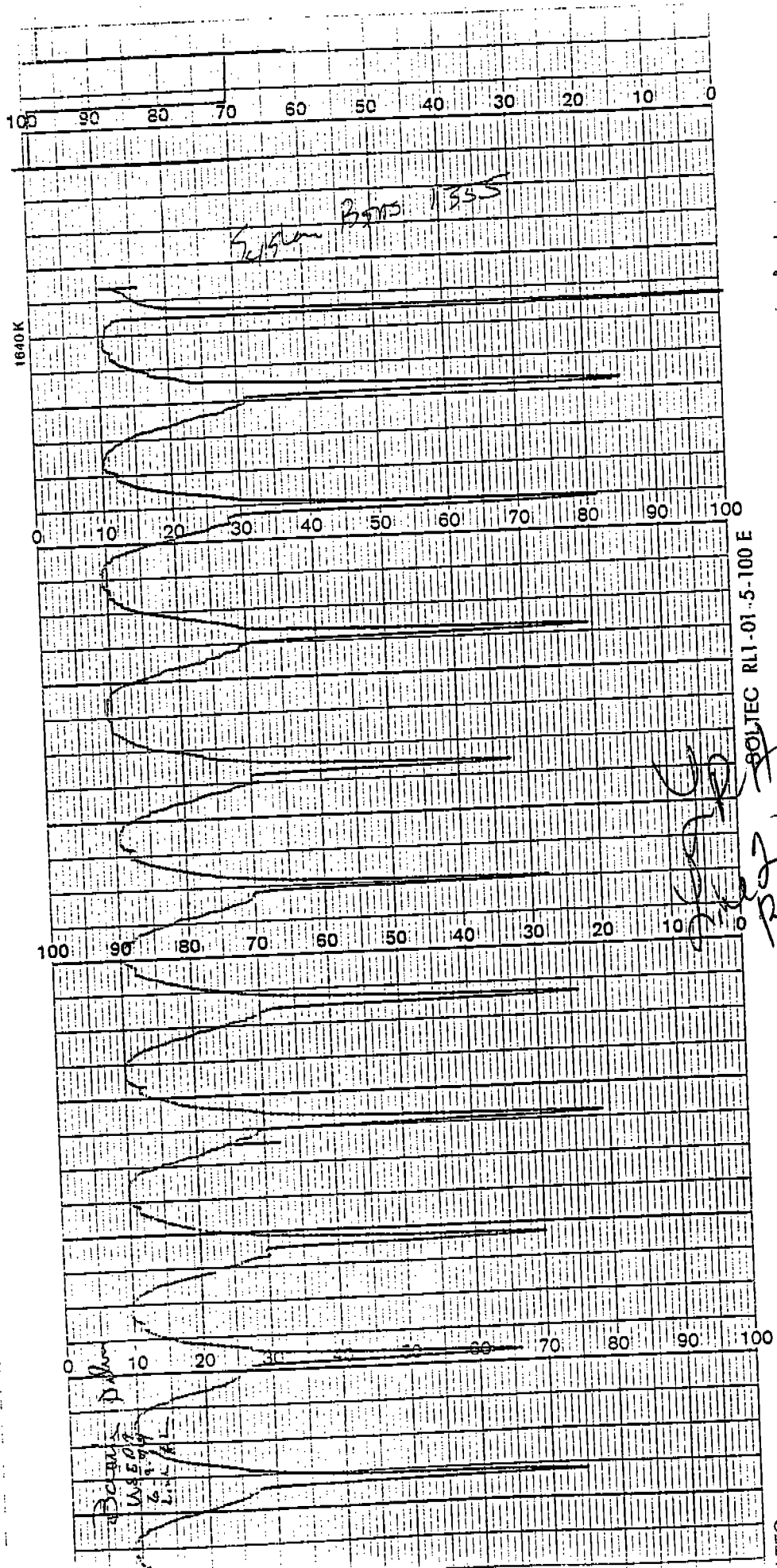
PRINTED IN U.S.A.

JP Hayward
9 PD Stack
HG-3





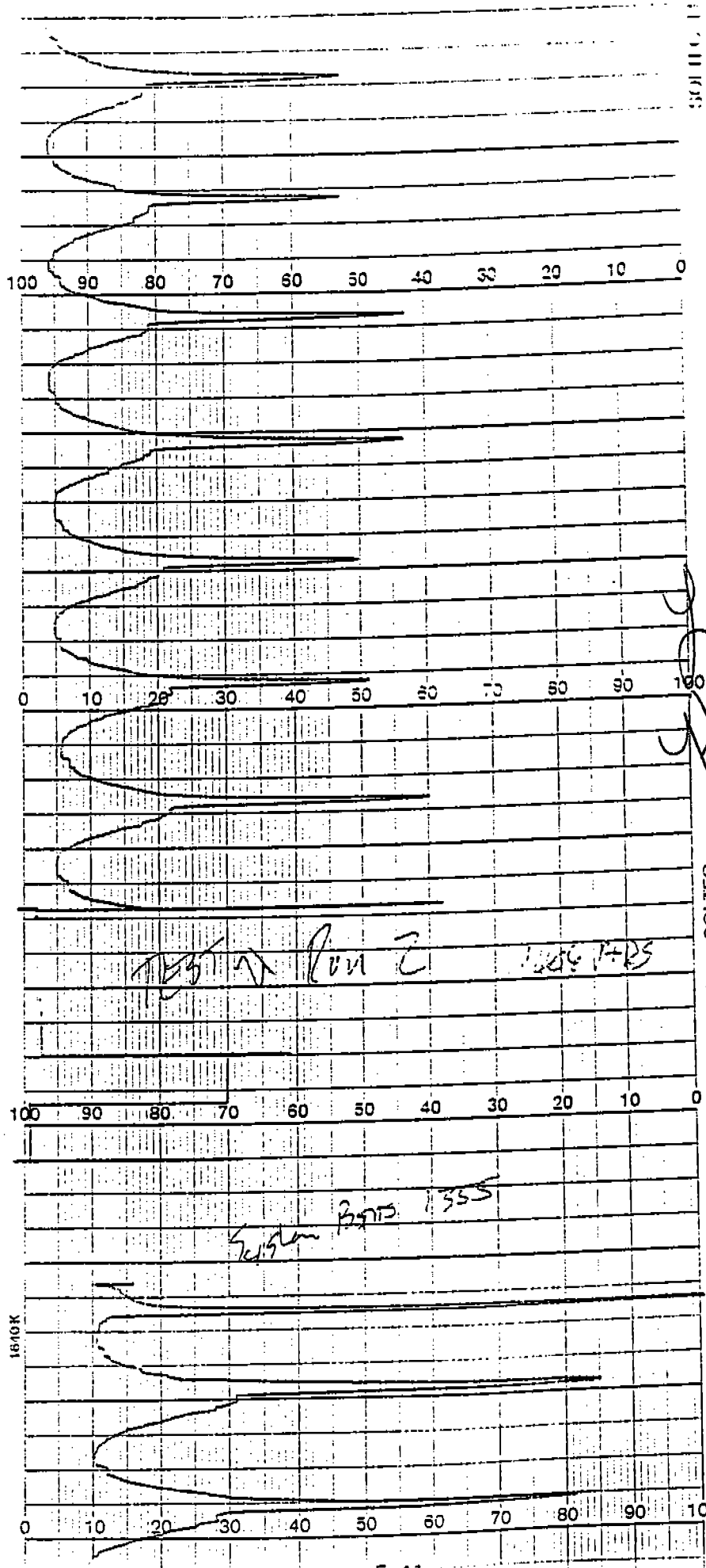
Handwritten:
 J.P. Hayward
 the 3
 not 21



90LITEC RL1-01.5-100 E

Hayward
2-Press
RTD Sulet

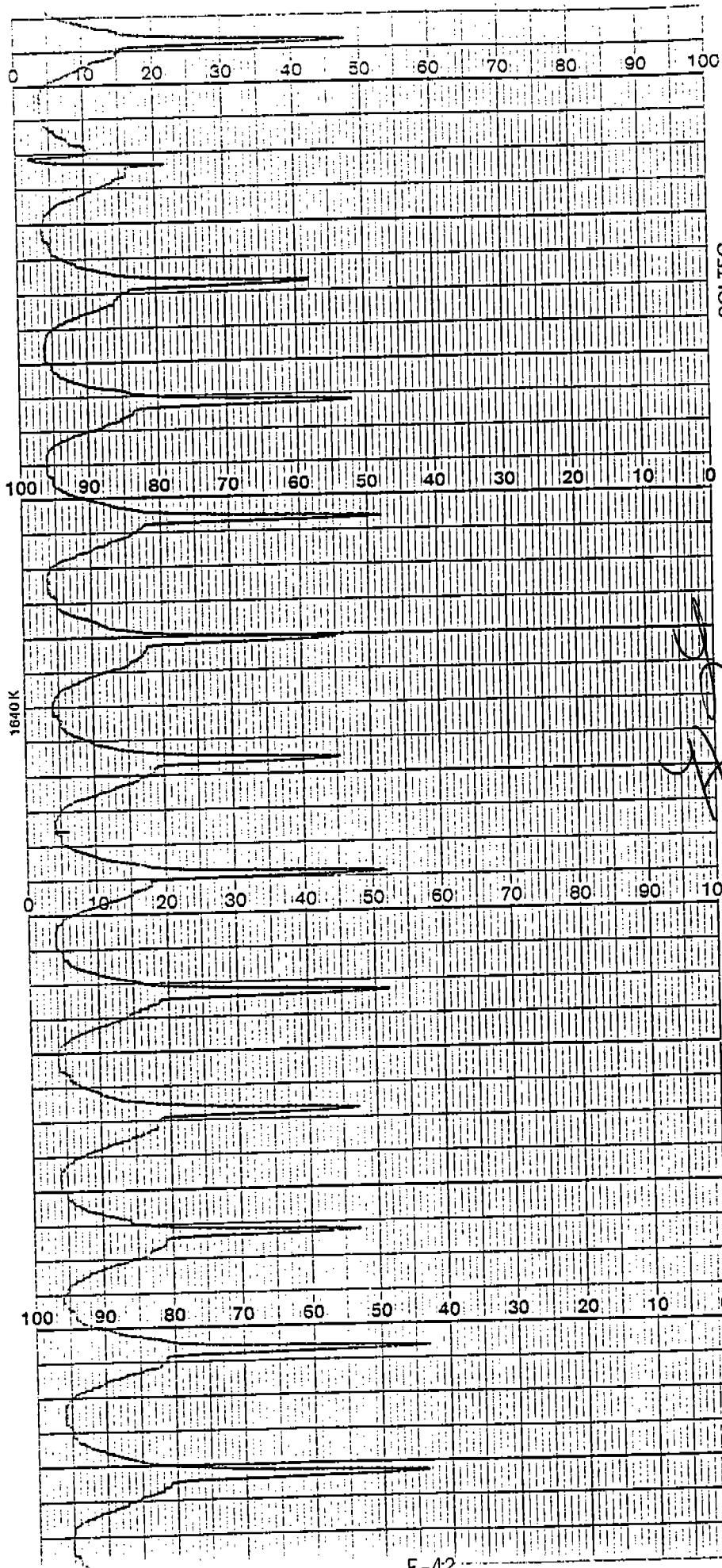
ALTEC



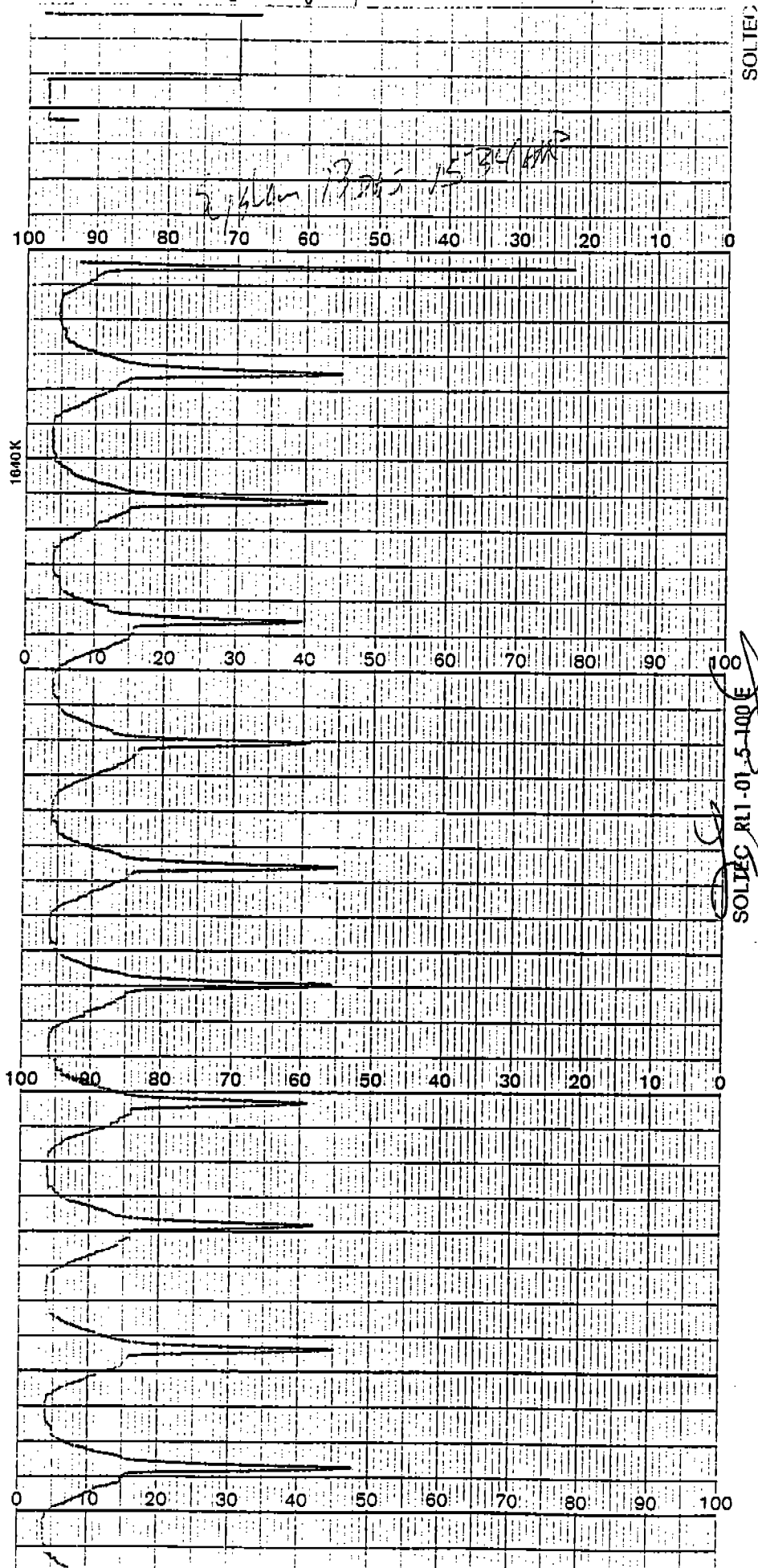
JP
Hayward
Test 21

1000 P+PS

1000 P+PS



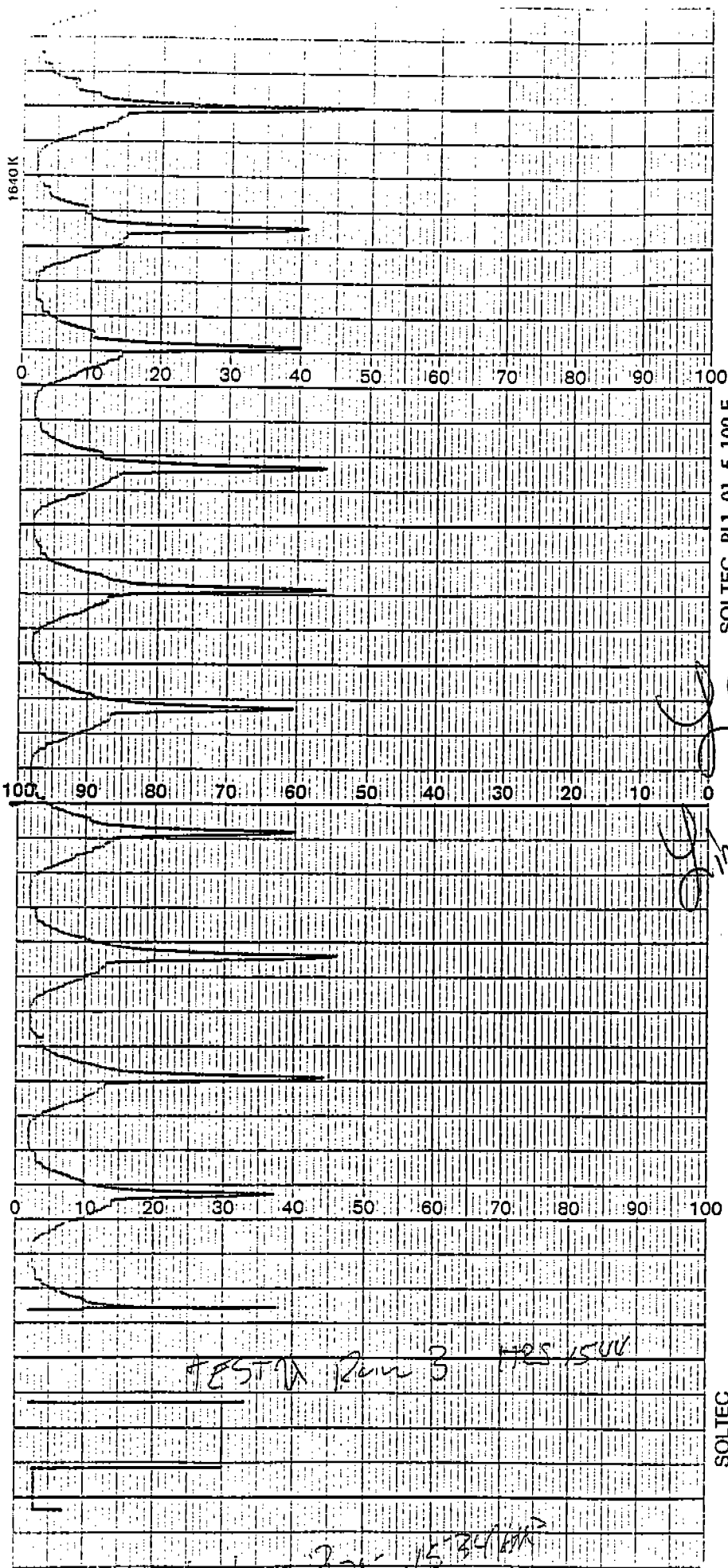
JP Hayward



SOLTEC

SOLTEC RL1-01.5-100 E

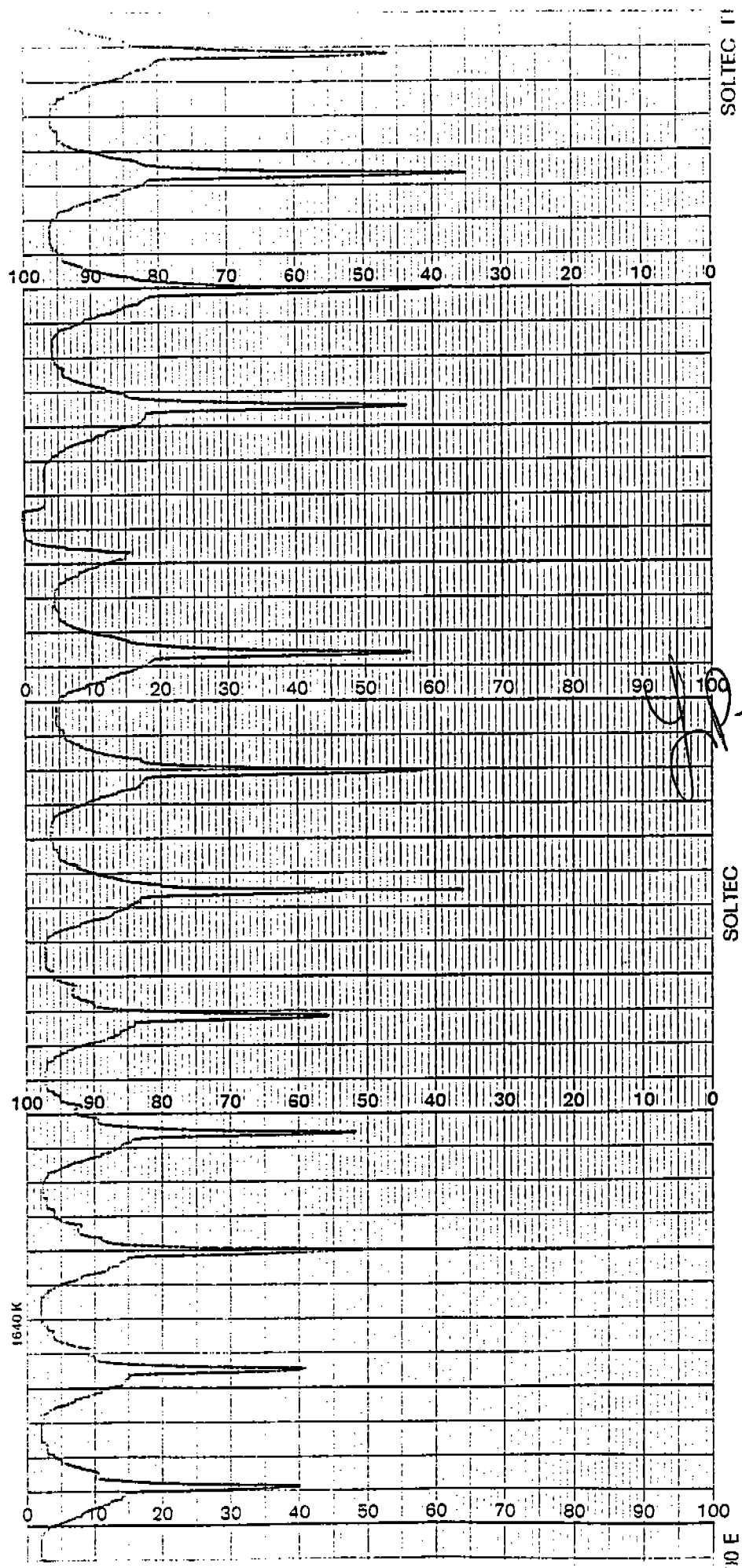
P. Hayward
the 2 Press
RTO Sulet



SOLTEC RL1-01-5-100 E

SOLTEC

J. R. Hayward
The 2. Pro
Pro Alert

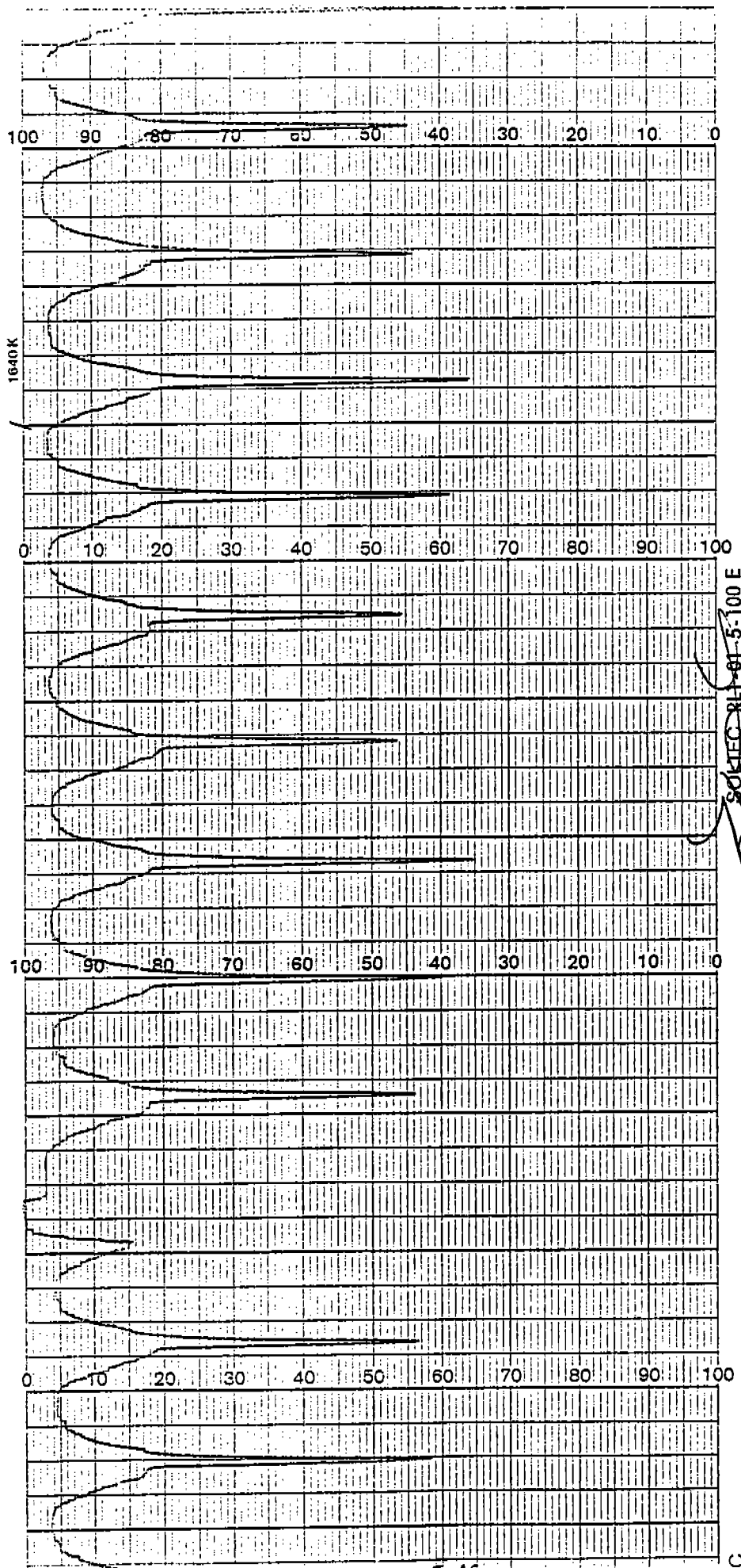


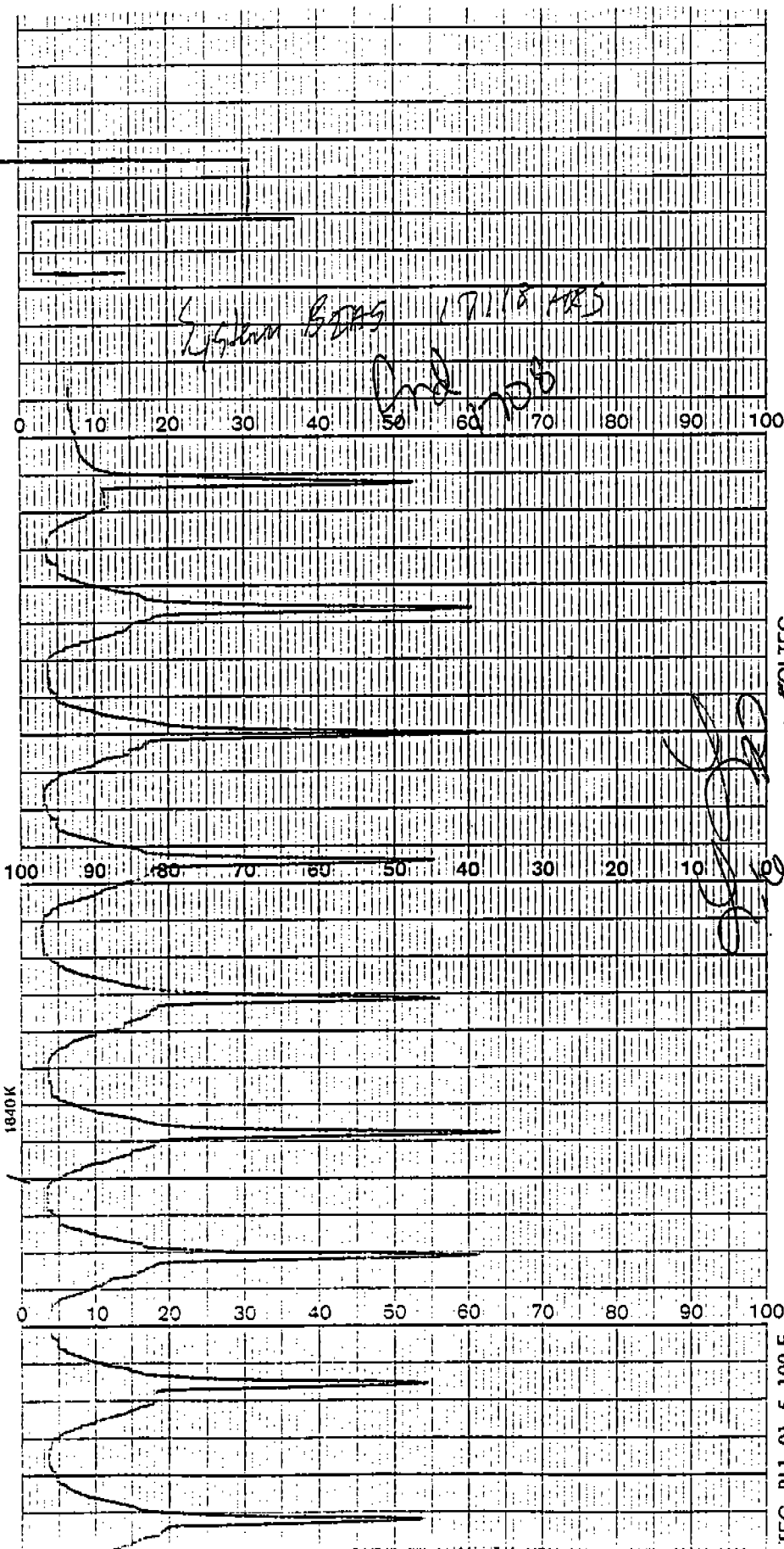
SOLTEC II

SOLTEC

30 F

F-45

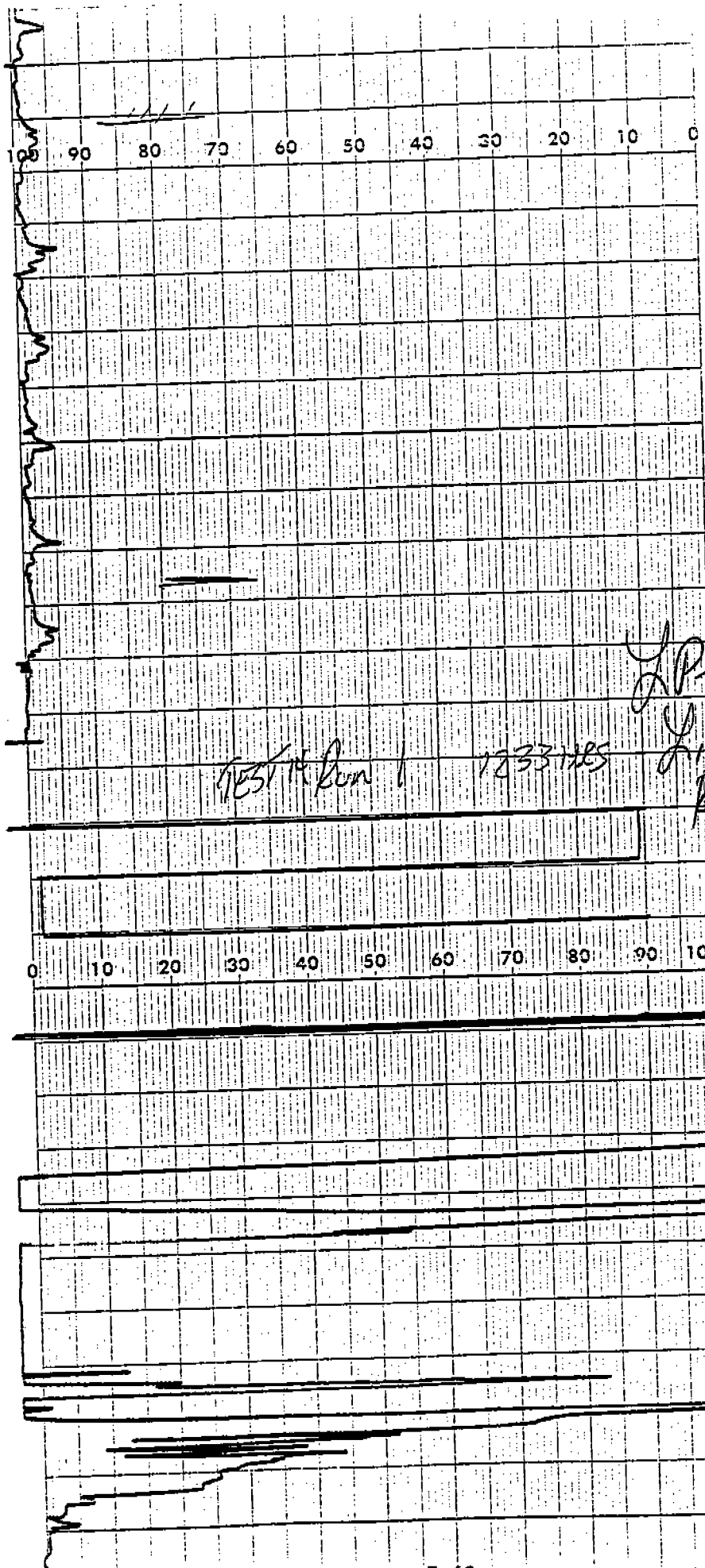




SOLTEC

Hayward
2 Pass
P.T.D. Inlet

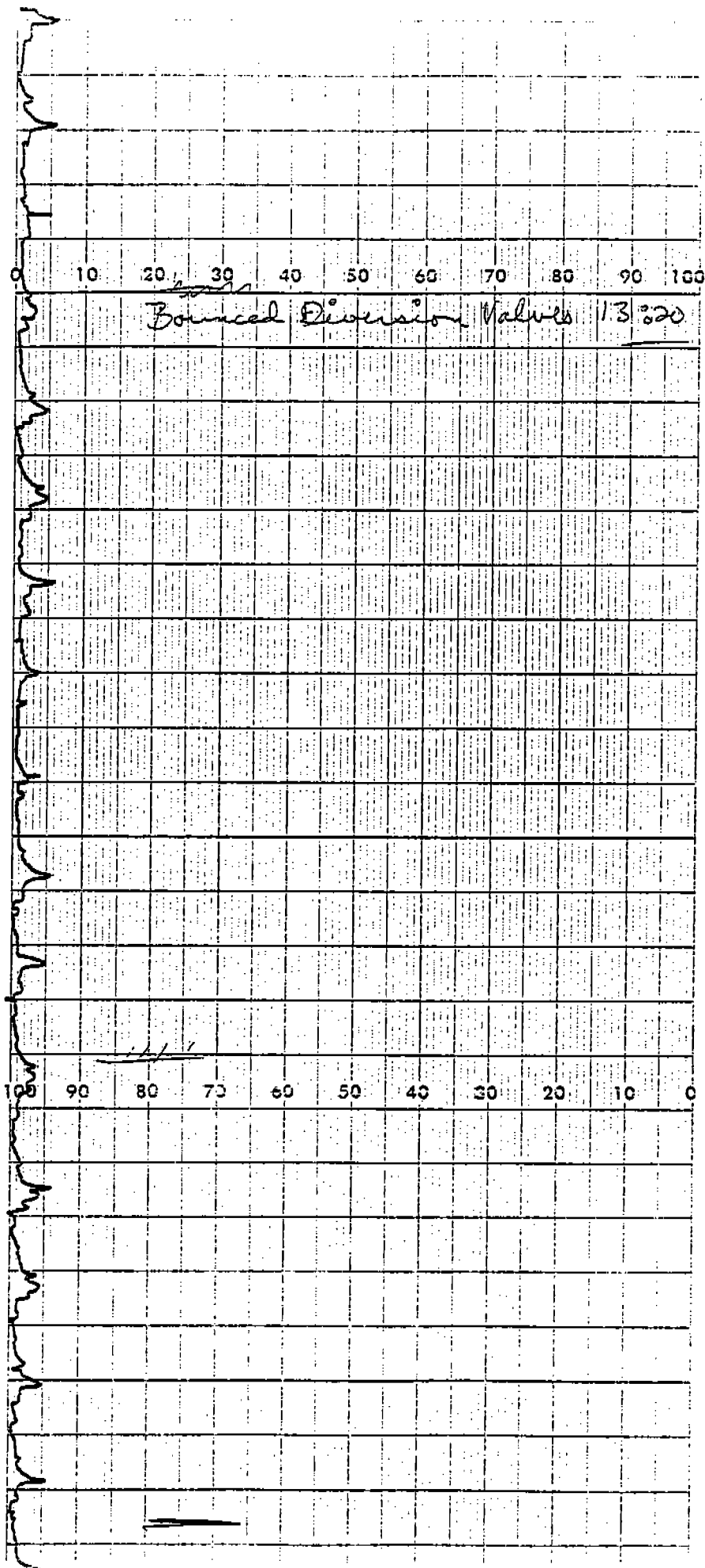
TEC RL1-01.5-100 E



GRAPHIC CONTROLS CORPORATION BUFFALO, NEW YORK

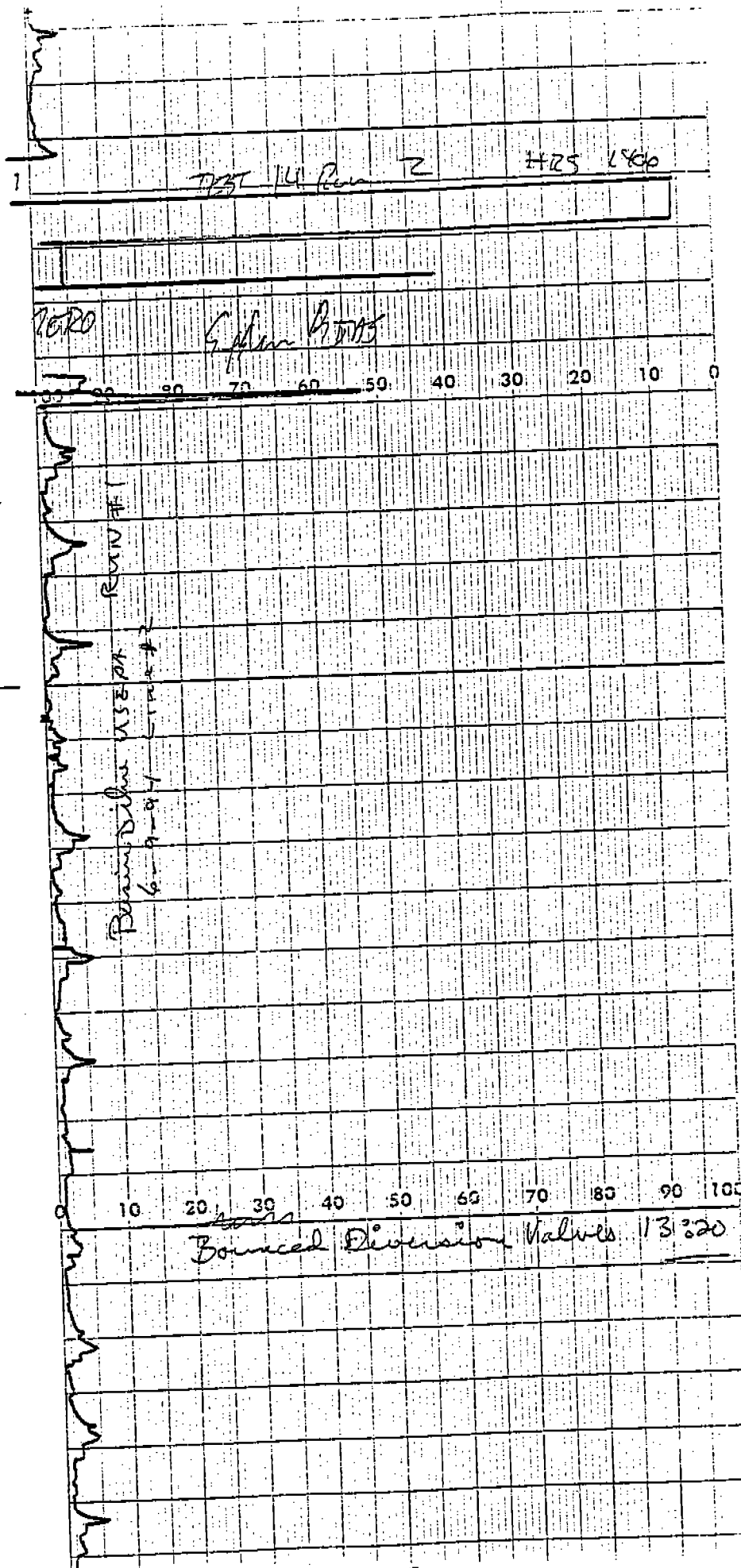
LP Hayward
Line 2 Press
BTO Stack

THC'S



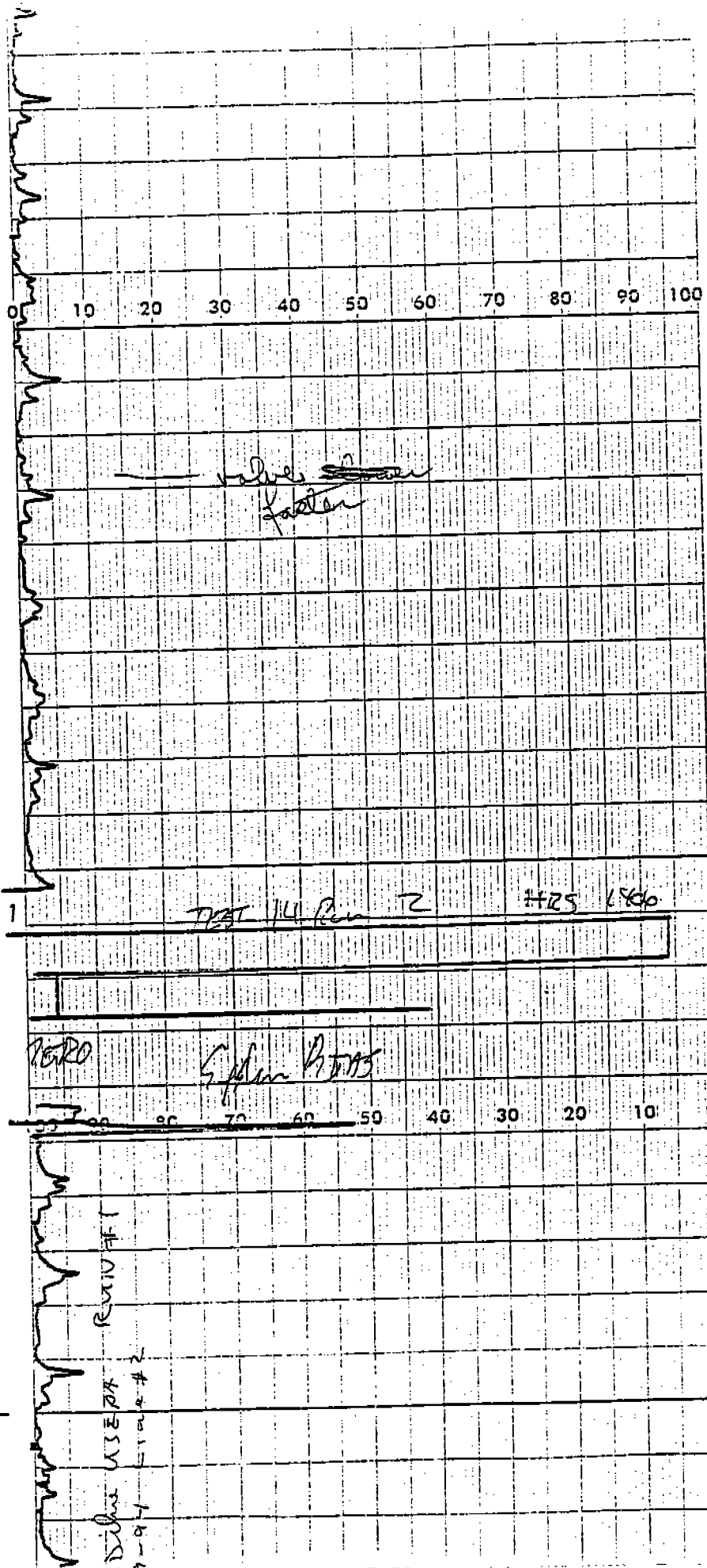
NO. IIR 0109 0917

GRAPHIC CONTROLS (CHIT) CANADA - BUFFALO, NEW YORK

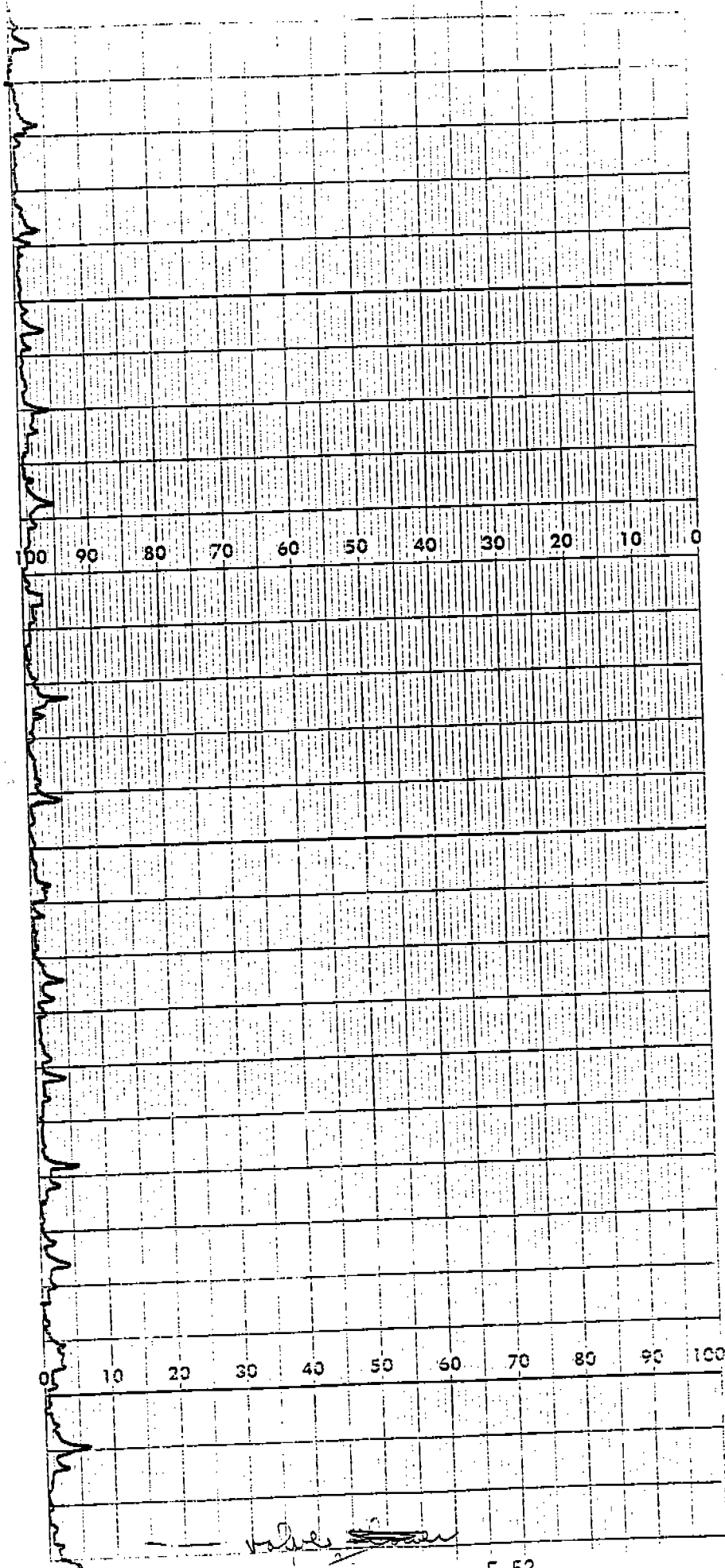


PROPERTY OF U.S. A.

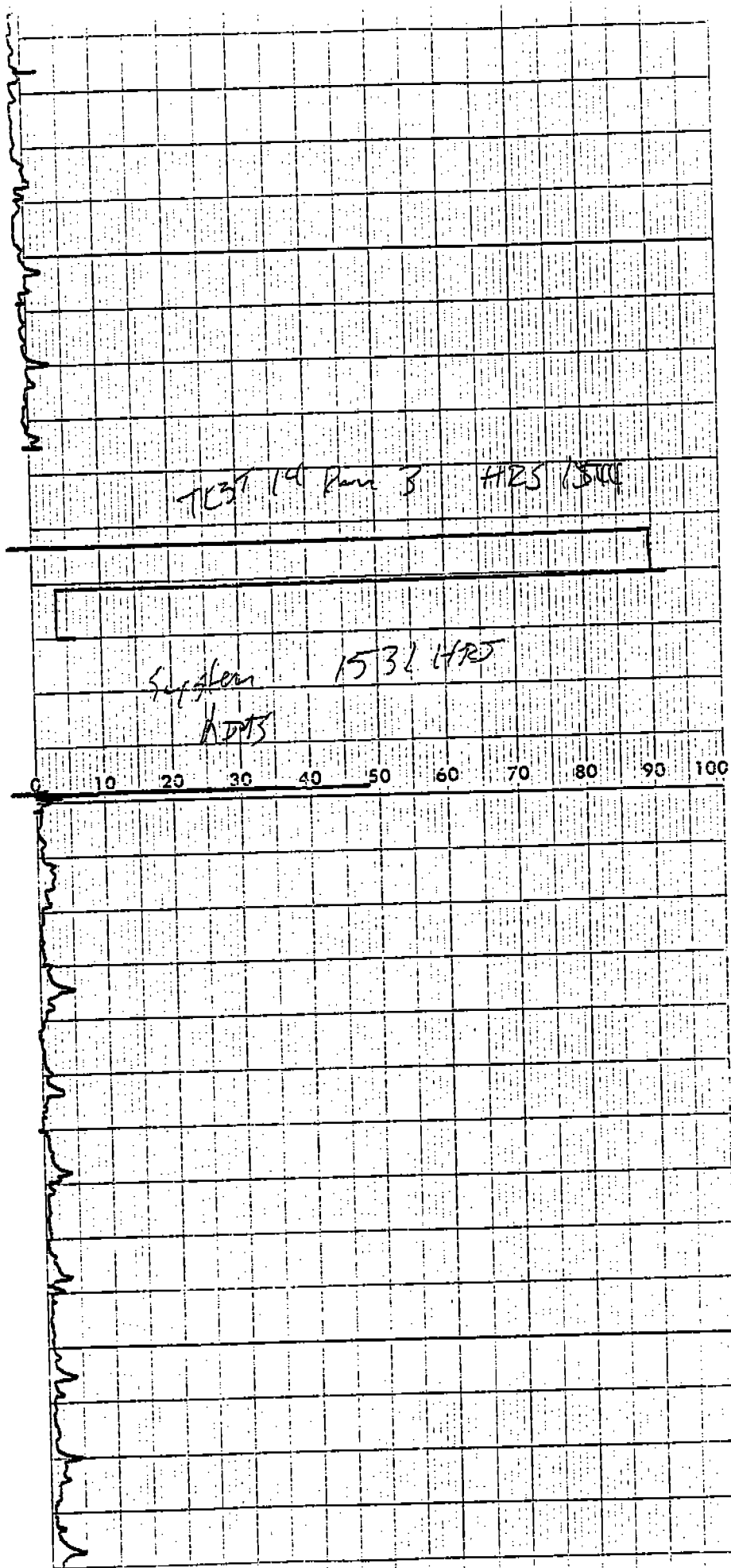
NO. LHR 0100.0017



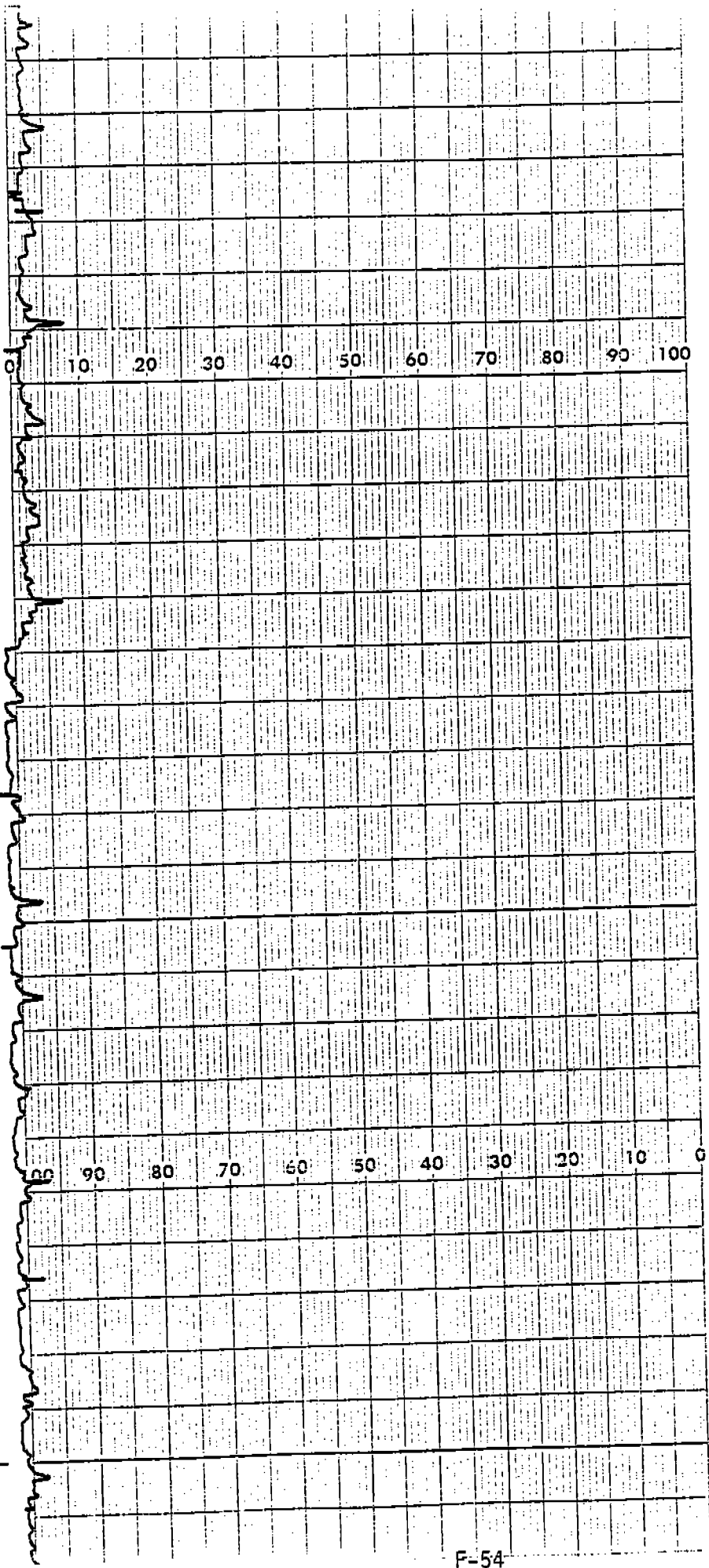
PRINTED IN U.S.A.



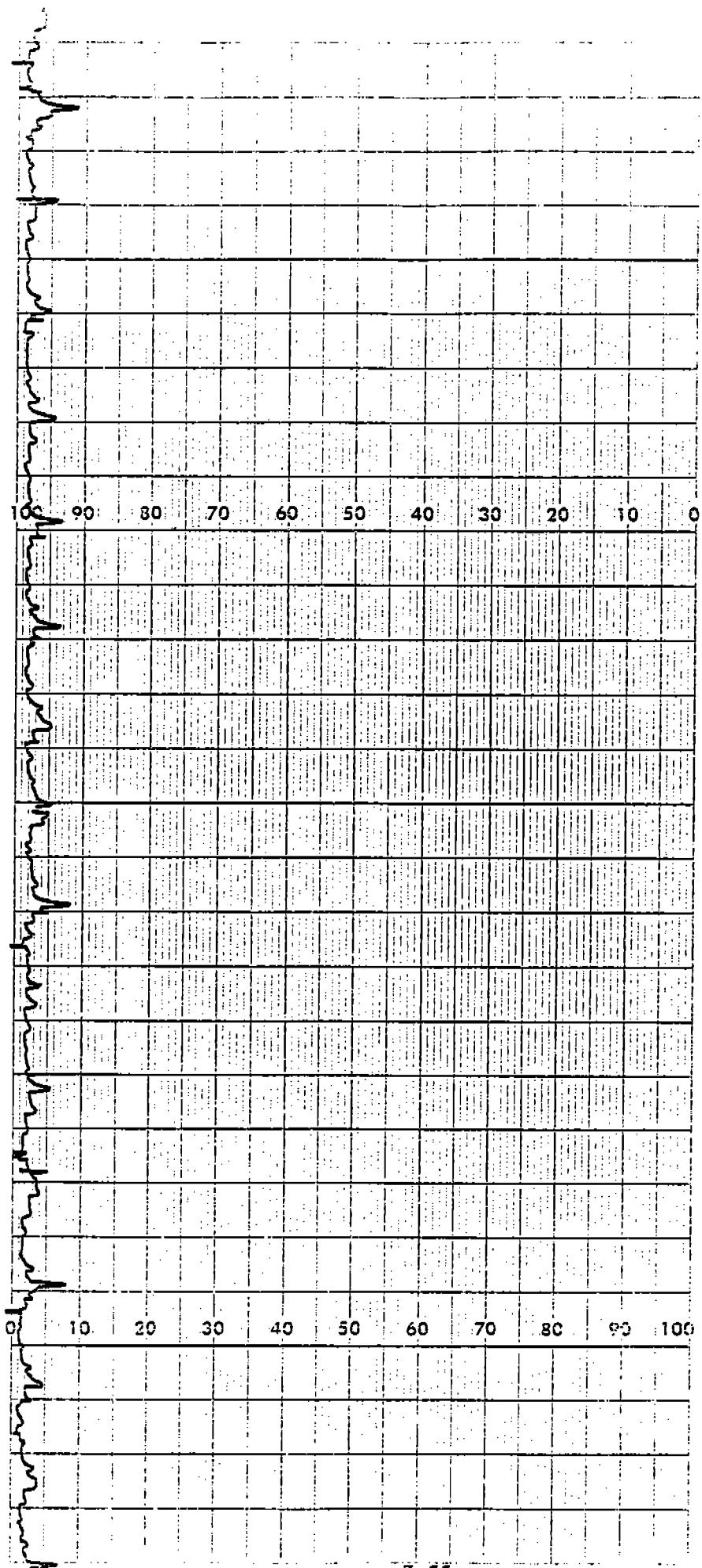
GRAPHIC CONTROLS CORPORATION BUFFALO, NEW YORK

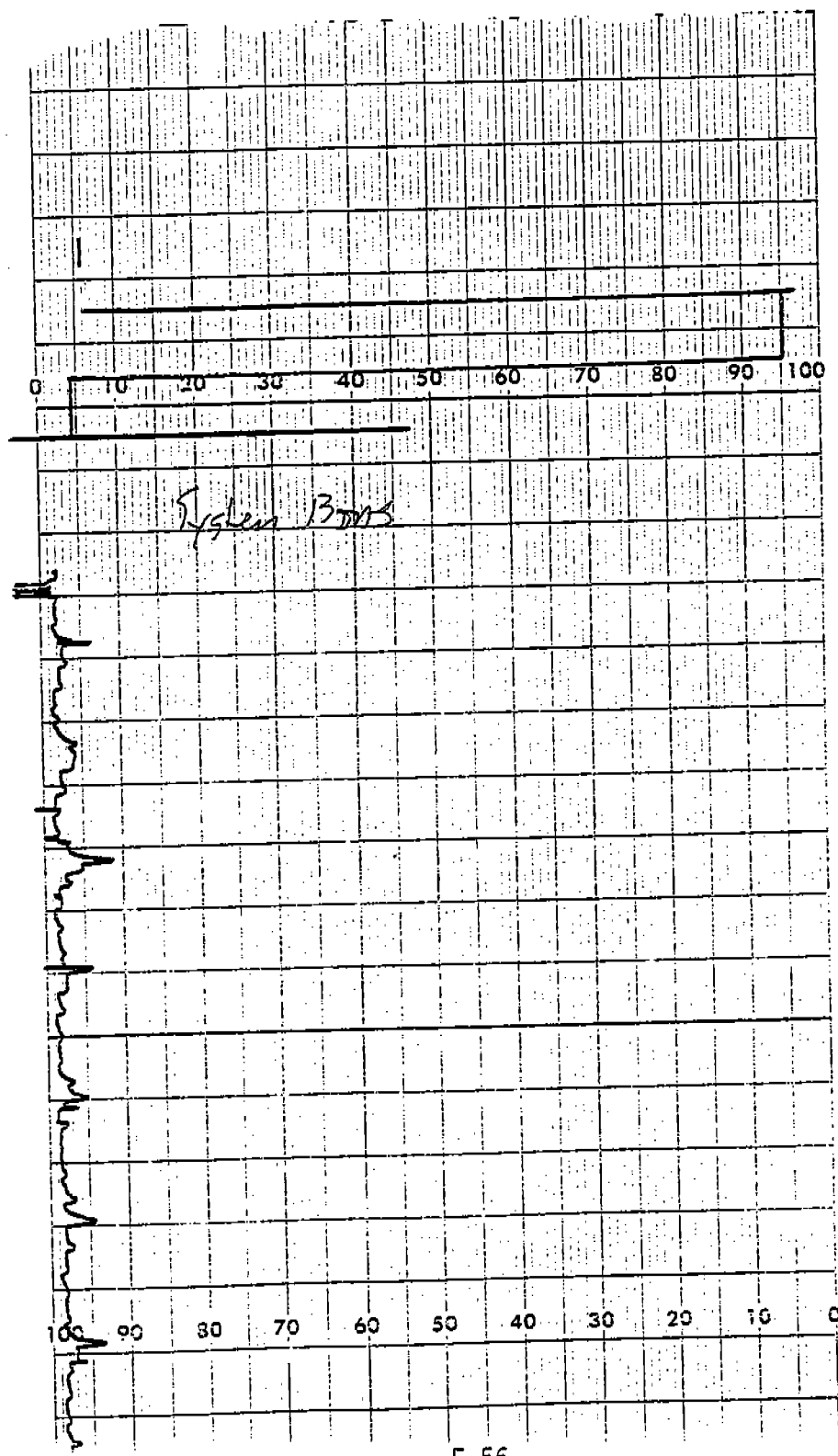


NO. INR 0100-0017



PRINTED IN U.S.A.





NO. INR 0100-0017

IRW BUFFALO, NEW YORK

APPENDIX G

ANALYZER SPECIFICATIONS



TOTAL HYDROCARBON ANALYZER (FLAME IONIZATION)
Model RS 55

TECHNICAL DATA

MAINS : 115V/60H

RECORDER OUTPUT : 0 - 5 V / 4-20mA

MODEL: X Manual switching
 — Solenoid valves

HOUSING: — Case, — 19" - Rack

MEASURING RANGES:	1 = 0 - 10	C ₁
	2 = 0 - 100	C ₁
	3 = 0 - 1,000	C ₁
	4 = 0 - 10,000	C ₁

SPECIAL OPTIONS :

Flame out alarm

1 Alarm

Sample line

.....

ANALYZER CONDITIONS:

Temperature : 160.°C

Zero Point : 3,90

Gain : 7,70

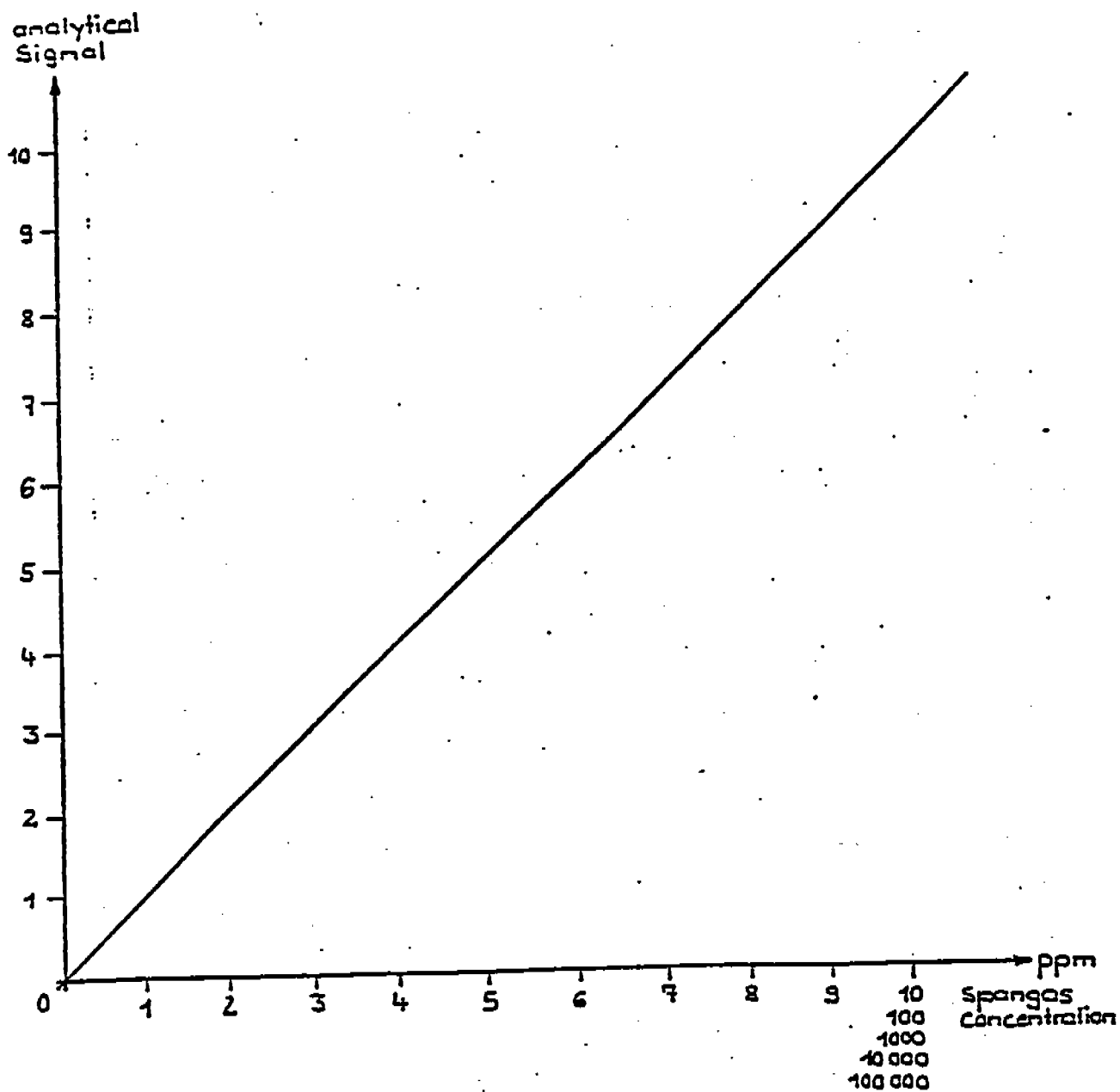
Pressure Setting: Sample/Spangas/Zerogas: 200 mbar

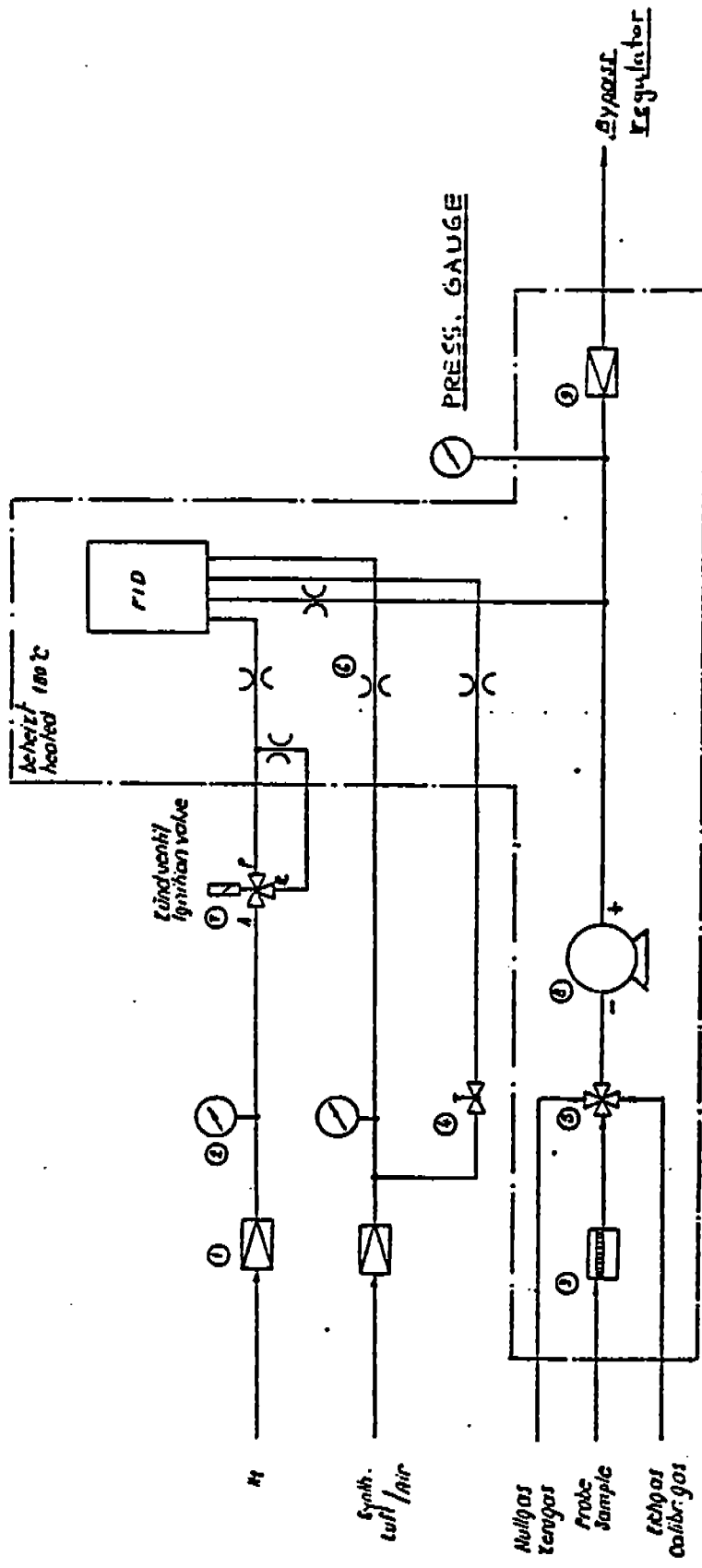
Fuel: Hydrogen : 0,35 bar

Combustion Air : 0,80 bar

Span Gases : 300. ppm C₁
 24.000. ppm C₁

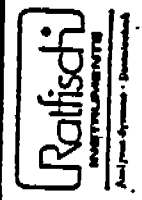
CALIBRATION DIAGRAMM





Zündventil
Ignition valve
P-A angezogen
energised
E-A startlos
at rest

- 1 Druckregler
pressure regulator
- 2 Manometer
Gauge
- 3 Filter
- 4 Nadelventil
needle valve
- 5 3 Wege Ventil
3 way valve
- 6 Kapillare
capillary
- 7 Magnetventil
magnet valve
- 8 Pumpe
pump
- 9 Rückdruckregler
back pressure regulator



Handumschaltung
manual switching

FLAMMEN IONISATIONS DETEKTOR
Flame Ionisation Detector

Fließplan
Flow diagram

RS 55

13.04.88

SPECIFICATIONS FOR ACS MODEL 3300 CO NDIR

Measuring principle	NDIR single beam method
Operating ranges	0 - 500 ppm 0 - 1000 ppm
Reproducibility	$\pm 0.5\%$ of full scale
Stability	Zero drift; $\pm 1\%$ of full scale/24H Span drift; $\pm 1\%$ of full scale/24H
Noise	0.5% of full scale
Ambient temperature	-5 to 45°C
Ambient humidity	Less than 90% RH
Response time (90% of final reading)	Electrical system; 2 sec, 3 sec, 5 sec (selectable with connector) Response of actual gas; Within 15 sec (depending on cell length)
Indicator	100 linear division
Output signal	OUTPUT 1; DC 0 - 1 V OUTPUT 2; DC 0 - 10 mV or DC 0 - 100 mV or DC 0 - 1 V or DC 4 - 20 mA (Allowable load resistance 500 Ω max.)
Linearity	Better than $\pm 2\%$ of full scale (when linearizer is used)
Power supply	AC 115 V $\pm 10\%$, 60 Hz

Power consumption	Approx. 30 VA
Materials of gas- contacting parts	Measuring cell; SUS304 Window; CaF ₂ Piping; Polyethylene
Sample gas flow rate	1ℓ/min ± 0.5ℓ/min
Sample gas temperature	0 to 55°C
Purging gas flow rate	1ℓ/min (to be flowed as occasion demands)
Warmup time	Approx. 2 hours
External dimensions	200 x 250 x 541 (H x W x D) mm
Weight	Approx. 11 kg
Finish Color	MUNSELL N1.5
Remarks:	For combinations of measuring ranges for the dualcomponent analyzer, inquiry should be made to the manufacturer.

SPECIFICATIONS FOR MODEL 10A
ROCK MOUNTED CHEMILUMINESCENT
NO-NO_x GAS ANALYZER

Sensitivity

Each instrument is equipped with the following ranges:

0 - 2.5 ppm
0 - 10 ppm
0 - 25 ppm
0 - 100 ppm
0 - 250 ppm
0 - 1000 ppm
0 - 2500 ppm
0 - 10000 ppm

Accuracy

Derived from the NO or NO₂ calibration gas, $\pm 1\%$ of fullscale

Response time (0-90%)
Typical

1.5 seconds - NO Mode
1.7 seconds - NO_x Mode

Output

0 - 10mV and 0 - 10V

Zero Drift

Negligible after 1/2-hour warm-up

Linearity

$\pm 1\%$ of full scale

Input Power Requirements

115v/50Hz; 115v/60Hz

Servomex

INTERPOL LABORATORIES
4500 BALL ROAD N.E.
CIRCLE PINES, MN 55014-1819
(612) 786-6020

1420 Oxygen Analyser Instruction Manual

Ref : 01420/001A/0

Order as part No. 01420001A

was (7982-2842)

INTERPOL LABORATORIES
4500 BALL ROAD N.E.
CIRCLE PINES, MN 55014-1819
(612) 786-6020

1.3 Sampling System

The sampling system of the analyser includes a combination filter/automatic flow control device, designed to keep a constant flow of sample gas through the measuring cell for varying input pressures and to prevent the entrance of particulate matter into the measuring cell. Excess flow is vented to the by-pass.

1.4 Specification

Performance Specification (typical)

Repeatability: Better than $\pm 0.2\%$ O₂ under constant conditions.

Drift: Less than 0.2% O₂ per week under constant conditions. (Excluding variation due to barometric pressure changes; reading is proportional to barometric pressure.)

Outputs

Display: 3 1/2 digit LCD reading 0.0 to 100.0% oxygen with overrange capability.

Output: 0 to 1V (non-isolated) for 0 to 100% oxygen available on 'D' type connector located on the back panel of the instrument. Output impedance is less than 10 ohms.

Option: 4 - 20mA isolated, Max impedance 500 ohms.

Flow alarm output: Change over relay contact rated at 3A/115V ac, 1A/240V ac or 1A/28V dc. 4 sets of single pole changeover contacts. Alarm becomes active when sample gas flow through the analyser fails.

Sample requirements

Condition: Clean, dry gas with dew point 5 deg C below ambient temperature.

Inlet pressure: 0.5 to 3psig (3.5 to 21kPa). Inlet pressure changes within this range will change the reading by less than 0.1% O₂. May be operated up to 10psig (70kPa) with degraded stability.

Flowrate: 1.5 to 6 litres/minute approximately depending on sample pressure.

Filtering: 0.6 micron replaceable filter integral to the automatic flow control device.

Response time: Less than 15 secs. to 90% at an inlet pressure of 3psig (21kPa).

Inlet/vent connections: 1/4 inch OD tube (stainless steel) suitable for 6mm ID flexible tubing or 1/4 inch OD compression fittings.

Materials exposed to the sample: Stainless steel, Pyrex glass, brass, platinum, epoxy resin, Viton, polypropylene and glass fibre filter.

Physical Characteristics

Case: Steel and aluminium finished in epoxy powder paint.

Case classification: IP 20 (IEC 529) when fitted into the Servomex 1400 series 19 inch case.

Dimensions: See Figure 2.1.

Weight: 10Kg (22lb) approximately.

Electrical

AC Supply: 110 to 120V AC or 220 to 240V AC, +/-10%, 48 to 62Hz. Voltage selected by a voltage selector integral to the IEC supply plug.

Power required: 15VA maximum.

Environmental Limits

Operating ambient temperature: 0 to +40 deg C (32 to 104 deg F)

Storage temp. range: -20 to +70 deg C (-4 to 158 deg F)

Relative humidity: 0-85%, non-condensing.

SPECIFICATIONS FOR ACS MODEL 3300 CO₂ NDIR

Measuring principle	NDIR single beam method
Measurable gas components and measuring range	0 - 20%
Reproducibility	±0.5% of full scale
Stability	Zero drift; ±% of full scale/24H Span drift; ±% of full scale/24H
Noise	0.5% of full scale
Ambient temperature	-5 to 45°C
Ambient humidity	Less than 90% RH
Response time (90% of final reading)	Electrical system; 2 sec, 3 sec, 5 sec (selectable with connector) Response of actual gas; Within 15 sec (depending on cell length)
Indicator	100 linear division
Output signal	OUTPUT 1; DC 0 - 1 V OUTPUT 2; DC 0 - 10 mV or DC 0 - 100 mV or DC 0 - 1 V or DC 4 - 20 mA (Allowable load resistance 500Ω max.)
Linearity	Better than ±2% of full scale (when linearizer is used)
Power supply	AC 115 V ± 10%, 60 Hz

Power consumption	Approx. 30 VA
Materials of gas-contacting parts	Measuring cell; SUS304 Window; CaF ₂ Piping; Polyethylene
Sample gas flow rate	1ℓ/min ± 0.5ℓ/min
Sample gas temperature	0 to 55°C
Purging gas flow rate	1ℓ/min (to be flowed as occasion demands)
Warmup time	Approx. 2 hours
External dimensions	200 x 250 x 541 (H x W x D) mm
Weight	Approx. 11 kg
Finish Color	MUNSELL N1.5

Remarks: For combinations of measuring ranges for the dualcomponent analyzer, inquiry should be made to the manufacturer.

APPENDIX H

MEASUREMENT SYSTEMS PERFORMANCE SPECIFICATIONS

INTERPOLL LABORATORIES, INC
(612) 786-6020

THC System Bias Check

Job LP/HAYWARD Source No 1 Press RTO
Test 1 Run 1-6 Date 7-24-86 Site STACCC
Operator BOB

Run	Time (HRS)	***	Cylinder Value (PPM)	Analyzer Resp (PPM)		Diff. CE-SB (PPM)	Span Val. (PPM)	% of Span
				Cal. Err.	Sys. Bias			
1	0721	Zero Gas	0	0	1	1	100	1
		Upscale	30	30	31	1	100	1
2	1040	Zero Gas	0	0	1	1	100	1
		Upscale	30	30	31	1	100	1
3	1209	Zero Gas	0	0	4	2	100	4
		Upscale	30	30	31	1	100	1
4	1323	Zero Gas	0	0	0	0	100	0
		Upscale	30	30	29	1	100	1
5		Zero Gas	0					
		Upscale						
6	0730	Zero Gas	0	0	2	2	100	2
		Upscale	91	91	90	1	100	1
7	1047	Zero Gas	0	0	3	2	100	3
		Upscale	91	91	92	2	100	3
8	1207	Zero Gas	0	0	4	4	100	4
		Upscale	91	91	92	1	100	1
9	1331	Zero Gas	0	0	3	3	100	3
		Upscale	91	91	91		100	
10		Zero Gas	0					
		Upscale						
11		Zero Gas	0					
		Upscale						
12		Zero Gas	0					
		Upscale						

Must be within 5% of the span for the zero or upscale cal. gas.

INTERPOLL LABORATORIES, INC

(612) 786-6020

NOx System Bias Check

Job

LP / HAYWARD

Source

Press No 1 RTO

Test

1 Run 1 - Date 6-7-94

Site

STACIC

Operator

BGB

Run	Time (HRS)	***	Cylinder Value (PPM)	Analyzer Resp (PPM)		Diff. CE-SB (PPM)	Span Val. (PPM)	% of Span
				Cal. Err.	Sys. Bias			
1	0756	Zero Gas	0	C	0	0	500	C
		Upscale	239	239	237	2	500	.40
2	0919	Zero Gas	0	0	1	1	500	.20
		Upscale	239	239	241	2	500	.40
3	1101	Zero Gas	0	0	0	0	500	0
		Upscale	239	239	239	0	500	0
4	1229	Zero Gas	0	0	1	1	500	.20
		Upscale	239	239	240	1	500	.20
5	0735	Zero Gas	0	0	1	1	100	1.0
		Upscale	78	76	76	0	100	0
6	1041	Zero Gas	0	0	0	0	100	0
		Upscale	78	76	76	0	100	0
7	1217	Zero Gas	0	0	1	1	100	1.0
		Upscale	78	76	74	0	100	0
8	1325	Zero Gas	0	0	3	-3	100	3
		Upscale	78	76	79	3	100	3
9		Zero Gas	0					
		Upscale						
10		Zero Gas	0					
		Upscale						
11		Zero Gas	0					
		Upscale						
12		Zero Gas	0					
		Upscale						

Must be within 3% of the span for the zero or upscale cal. gas.

033194-G:STACKIWPAFORMSS-420-11

INTERPOLL LABORATORIES, INC
(612) 786-6020

02 System Bias Check

Job LP / HAYWARD Source Press No 1 RTO
Test 1 Run 1 Date 6-7-84 Site STACIC
Operator BBB

Run	Time (HRS)	***	Cylinder Value (PPM)	Analyzer Resp (PPM)		Diff. CE-SB (PPM)	Span Val. (PPM)	% of Span
				Cal. Err.	Sys. Bias			
1	0750	Zero Gas	0	0	.1	.1	25	.40
		Upscale	13.5	13.4	13.5	.1	25	.40
2	0919	Zero Gas	0	0	0	0	25	0
		Upscale	13.5	13.4	13.5	.1	25	.40
3	1101	Zero Gas	0	0	0	0	25	0
		Upscale	13.5	13.4	13.4	0	25	0
4	1229	Zero Gas	0	0	0	0	25	0
		Upscale	13.5	13.4	13.5	.1	25	.40
5	0735	Zero Gas	0	0	0	0	25	0
		Upscale	13.5	13.4	13.4	0	25	0
6	1041	Zero Gas	0	0	0	0	25	0
		Upscale	13.5	13.4	13.5	.1	25	.40
7	1217	Zero Gas	0	0	.1	.1	25	.40
		Upscale	13.5	13.4	13.5	.1	25	.40
8		Zero Gas	0	0	0	0	25	0
		Upscale	12.5	13.4	13.6	.2	25	.80
9		Zero Gas	0					
		Upscale						
10		Zero Gas	0					
		Upscale						
11		Zero Gas	0					
		Upscale						
12		Zero Gas	0					
		Upscale						

Must be within 5% of the span for the zero or upscale cal. gas.

BBB
6/7/84

INTERPOLL LABORATORIES, INC

(612) 786-6020

CO₂ System Bias Check

Job LP / HAYWARD Source Press No 1 RTO
 Test 1 Run 1 Date 6-7-84 Site STACIC
 Operator BBB

Run	Time (HRS)	***	Cylinder Value (PPM)	Analyzer Resp (PPM)		Diff. CE-SB (PPM)	Span Val. (PPM)	% of Span
				Cal. Err.	Sys. Bias			
1	0756	Zero Gas	0	0	0	0	20	0
		Upscale	11.1	11.0	11.0	0	20	0
2	0919	Zero Gas	0	0	.1	-.1	20	.50
		Upscale	11.1	11.0	11.0	0	20	0
3	1101	Zero Gas	0	0	0	0	20	0
		Upscale	11.1	11.0	10.9	-.1	20	.56
4	1229	Zero Gas	0	0	0	0	20	0
		Upscale	11.1	11.0	10.9	-.1	20	.50
5	0735	Zero Gas	0	0	.1	-.1	20	.50
		Upscale	11.1	11.0	11.0	0	20	0
6	1041	Zero Gas	0	0	.1	-.1	20	.50
		Upscale	11.1	11.0	11.1	.1	20	.50
7	1217	Zero Gas	0	0	.1	-.1	20	.50
		Upscale	11.1	11.0	11.1	.1	20	.50
8		Zero Gas	0	0	0	0	20	0
		Upscale	11.1	11.0	11.1	-.1	20	.50
9		Zero Gas	0					
		Upscale						
10		Zero Gas	0					
		Upscale						
11		Zero Gas	0					
		Upscale						
12		Zero Gas	0					
		Upscale						

Must be within 5% of the span for the zero or upscale cal. gas.

Barium Doh
6/8/84

033194-GASTACKWP\FORMS\S-420-11

INTERPOLL LABORATORIES, INC

(612) 786-6020

CO System Bias Check

Job

CP/ HAYWARD

Source

PRESS No 1 RTG

Test

1 Run 1Date 6-7-94

Site

STACK

Operator

Bob

Run	Time (HRS)	***	Cylinder Value (PPM)	Analyzer Resp (PPM)		Diff. CE-SB (PPM)	Span Val. (PPM)	% of Span
				Cal. Err.	Sys. Bias			
1	0919	Zero Gas	0	0	0	0	500	0
		Upscale	159	159	155	4	500	.80
2	1001	Zero Gas	0	0	2	2	500	.40
		Upscale	159	159	154	5	500	1.00
3	1229	Zero Gas	0	0	2	2	500	.40
		Upscale	159	159	155	4	500	.80
4		Zero Gas	0					
		Upscale						
5	0735	Zero Gas	0	0	1	1	500	.20
		Upscale	159	159	158	1	500	.20
6	1041	Zero Gas	0	0	3	3	500	.60
		Upscale	159	159	166	1	500	.20
7	1217	Zero Gas	0	0	3	3	500	.60
		Upscale	159	159	155	4	500	.80
8		Zero Gas	0	0	4	4	500	.80
		Upscale	159	159	154	5	500	1.00
9		Zero Gas	0					
		Upscale						
10		Zero Gas	0					
		Upscale						
11		Zero Gas	0					
		Upscale						
12		Zero Gas	0					
		Upscale						

Must be within 5% of the span for the zero or upscale cal. gas.

Baird
45872

033194-G:\STACK\WP\FORMS\G-20-11

INTERPOLL LABORATORIES, INC

(612) 786-6020

EPA Method 25 A

Calibration Error Check & Drift Determination

Job

Test

Operator

CP / HAYWARD - Line 1 RTO inlet
 Run 0 Date 6-6-84
 Operator BBB

THC Calibration (Low Range):

Time (HRS) _____

***	Cylinder Value (PPM)	Analyzer Response (PPM)	Difference (PPM)	Span Value (PPM)	Percent Of Span
Zero Gas	0	0	0	100	5
Low Level	30.3 ⁹¹	91		100	
Mid Level	303 ⁹¹⁰	910		1000	
High Level	3038 ⁹¹⁰⁰			10000	

THC Calibration (High Range):

Time (HRS) _____

***	Cylinder Value (PPM)	Analyzer Response (PPM)	Difference (PPM)	Span Value (PPM)	Percent Of Span
Zero Gas	0				
Span					

O₂ Calibration:

Time (HRS) _____

***	Cylinder Value (%)	Analyzer Response (%)	Difference (%)	Span Value (%)	Percent Of Span
Zero Gas	0				
Mid Level					
High Level					

CO₂ Calibration:

Time: (HRS) _____

***	Cylinder Value (%)	Analyzer Response (%)	Difference (%)	Span Value (%)	Percent Of Span
Zero Gas	0				
Mid Level					
High Level					

Must be within 2% or the span for each calibration gas.

INTERPOLL LABORATORIES, INC

(612) 786-6020

System Bias Check

Job

LP/HAYWARD

Source

Test

Run

Date

Site

Operator

Run	Time (HRS)	***	Cylinder Value (PPM)	Analyzer Resp (PPM)		Diff. CE-SB (PPM)	Span Val. (PPM)	% of Span
				Cal. Err.	Sys. Bias			
1	0730	Zero Gas	0	0	0	0	100	0
		Upscale	30.3	30	30	0	100	0
2	0916	Zero Gas	0	0	0	0	100	0
		Upscale	30.3	30	30	0	100	0
3	1058	Zero Gas	0	0	2	2	100	
		Upscale	30.3	30	31	1	100	
4	1227	Zero Gas	0	0	2	2	100	
		Upscale	30.3	30	32	2	100	
5		Zero Gas	0					
		Upscale						
6		Zero Gas	0					
		Upscale						
7		Zero Gas	0					
		Upscale						
8		Zero Gas	0					
		Upscale						
9		Zero Gas	0					
		Upscale						
10		Zero Gas	0					
		Upscale						
11		Zero Gas	0					
		Upscale						
12		Zero Gas	0					
		Upscale						

Must be within 5% of the span for the zero or upscale cal. gas.

033194-GASTACKWPFORMSS-20-11

INTERPOLL LABORATORIES, INC

(612) 786-6020

EPA Method 25 A

Calibration Error Check & Drift Determination

Job

Test

Operator

LD. Hayward - Line 1 RTD Stack

Run

Date

THC Calibration (Low Range):

Time (HRS) _____

***	Cylinder Value (PPM)	Analyzer Response (PPM)	Difference (PPM)	Span Value (PPM)	Percent Of Span
Zero Gas	0	0	0	100	0
Low Level	303	30	3	100	
Mid Level	303	300		1000	
High Level	3030	3050		10000	

THC Calibration (High Range):

Time (HRS) _____

***	Cylinder Value (PPM)	Analyzer Response (PPM)	Difference (PPM)	Span Value (PPM)	Percent Of Span
Zero Gas	0				
Span					

O₂ Calibration:

Time (HRS) _____

***	Cylinder Value (%)	Analyzer Response (%)	Difference (%)	Span Value (%)	Percent Of Span
Zero Gas	0				
Mid Level					
High Level					

CO₂ Calibration:

Time: (HRS) _____

***	Cylinder Value (%)	Analyzer Response (%)	Difference (%)	Span Value (%)	Percent Of Span
Zero Gas	0				
Mid Level					
High Level					

Must be within 2% of the span for each calibration gas.

121593-G:STACK/WP/FORMS/420-14

INTERPOLL LABORATORIES, INC

(612) 786-6020

TTC System Bias Check

Job

LP/HAYWARD

Source

Test

Run

Date

Site

Operator

Run	Time (HRS)	***	Cylinder Value (PPM)	Analyzer Resp (PPM)		Diff. CE-SB (PPM)	Span Val. (PPM)	% of Span
				Cal. Err.	Sys. Bias			
1	0735	Zero Gas	0	0	0	0	106	6
		Upscale	91.0	91	91	0	100	0
2	0927	Zero Gas	0	0	0	0	100	0
		Upscale	91.0	91	91	0	100	0
3	1055	Zero Gas	0	0	4	4	100	4.0
		Upscale	91.0	91	94	3	100	
4	1237	Zero Gas	0	0	3			
		Upscale	91.0	91	90			
5		Zero Gas	0					
		Upscale						
6		Zero Gas	0					
		Upscale						
7		Zero Gas	0					
		Upscale						
8		Zero Gas	0					
		Upscale						
9		Zero Gas	0					
		Upscale						
10		Zero Gas	0					
		Upscale						
11		Zero Gas	0					
		Upscale						
12		Zero Gas	0					
		Upscale						

Must be within 5% or the span for the zero or upscale cal. gas.

03319-GASTACK\WP\FORMS-420-11

INTERPOL LABORATORIES

Calibration Error Check

Job WHEELABRATOR LP/HAYWARD

Test _____ Run _____ Date _____

Operator _____

CO~~NO~~ Calibration:

Time (HRS) _____

***	Cylinder Value (ppm)	Analyzer Response (ppm)	Difference (ppm)	Span Value (ppm)	Percent of Span
Zero gas	0	5	5	500	
Mid level	159	159	0	500	0
High level	249	252	3	500	

CO~~NO~~ Calibration:

Time (HRS) _____

***	Cylinder Value (ppm)	Analyzer Response (ppm)	Difference (ppm)	Span Value (ppm)	Percent of Span
Zero gas	0	2	2	500	
Mid level	159	155	4	500	
High level	249	250	0	500	

O₂ Calibration:

Time (HRS) _____

***	Cylinder Value (ppm)	Analyzer Response (ppm)	Difference (ppm)	Span Value (ppm)	Percent of Span
Zero gas	0	.1	.1	25	.40
Mid level	13.5	13.5	0	25	0
High level	21.0	21.1	.1	25	.40

CO₂ Calibration:

Time (HRS) _____

***	Cylinder Value (ppm)	Analyzer Response (ppm)	Difference (ppm)	Span Value (ppm)	Percent of Span
Zero gas	0	.1	.1	20	.50
Mid level	11.1	11.0	.1	20	.50
High level	17.0	17.1	.1	20	.50

Must be within 2% of the span for each calibration gas

S-420-10

INTERPOLL LABORATORIES, INC

(612) 786-6020

EPA Method 25 A

Calibration Error Check & Drift Determination

Job

LP 1/HAYWARD

Line 2 Press RTD Stack

Test

Run

Date 6-8-84

Operator

BOS

VOC

THC Calibration (Low Range):

Time (HRS)

***	Cylinder Value (PPM)	Analyzer Response (PPM)	Difference (PPM)	Span Value (PPM)	Percent Of Span
Zero Gas	0	0	0	100	0
Low Level	91	91	0	100	0
Mid Level	910	910	0	1000	0
High Level	9100	9100	0	10000	0

THC Calibration (High Range):

Time (HRS)

***	Cylinder Value (PPM)	Analyzer Response (PPM)	Difference (PPM)	Span Value (PPM)	Percent Of Span
Zero Gas	0				
Span					

O₂ Calibration:

Time (HRS)

***	Cylinder Value (%)	Analyzer Response (%)	Difference (%)	Span Value (%)	Percent Of Span
Zero Gas	0				
Mid Level					
High Level					

CO₂ Calibration:

Time: (HRS)

***	Cylinder Value (%)	Analyzer Response (%)	Difference (%)	Span Value (%)	Percent Of Span
Zero Gas	0				
Mid Level					
High Level					

Must be within 2% of the span for each calibration gas.

121593-G:\STACK\WP\FORMS\S-420-14

INTERPOL LABORATORIES, INC

(612) 786-6020

THC System Bias Check

Job

CP/HAYWARD

Source

LTLR 2 Press RR

Test

Run

Date

6-8-74
6-8-74

Site

STACK

Operator

603

Run	Time (HRS)	***	Cylinder Value (PPM)	Analyzer Resp (PPM)		Diff. CE-SB (PPM)	Span Val. (PPM)	% of Span
				Cal. Err.	Sys. Bias			
1		Zero Gas	0	0	0	0	100	5
		Upscale	91	94	90	4	100	10
2	A03	Zero Gas	0	0	0	0	100	0
		Upscale	91	91	91	0	100	0
3	0723	Zero Gas	0	0	0	0	100	0
		Upscale	91	91	91	0	100	0
4	0826	Zero Gas	0	0	8	8	100	8.0
		Upscale	91	91	87	4	100	4.0
5	0824	Zero Gas	0	0	0	0	100	0
		Upscale	91	91	90	1.0	100	1.0
6	1035	Zero Gas	0	0	2	2	100	2.0
		Upscale	91	91	91	0	100	0
7	1400	Zero Gas	0	0	4	4	100	4.0
		Upscale	91	91	94	3	100	3.0
8	1531	Zero Gas	0	0	4	4	100	4.0
		Upscale	91	91	90	1	100	1.0
9	1926	Zero Gas	0	0	4	4	100	4.0
		Upscale	91	91	94	3	100	3.0
10		Zero Gas	0					
		Upscale						
11		Zero Gas	0					
		Upscale						
12		Zero Gas	0					
		Upscale						

Must be within 5% of the span for the zero or upscale cal. gas.

033194-G:STACKIWPFORMSIS-120-11

INTERPOL LABORATORIES, INC

(612) 786-6020

EPA Method 25 A

Calibration Error Check & Drift Determination

Job

CP / HAYWARD

Line 2 RTD Inlet

Test

Run

Date

Operator

RBB

THC Calibration (Low Range):

Time (HRS)

***	Cylinder Value (PPM)	Analyzer Response (PPM)	Difference (PPM)	Span Value (PPM)	Percent Of Span
Zero Gas	0	1	1	100	1.0
Low Level	30.3	30	.3	100	.3
Mid Level	303	300	3	1000	.3
High Level	3038	3030	8	10000	.8

THC Calibration (High Range):

Time (HRS)

***	Cylinder Value (PPM)	Analyzer Response (PPM)	Difference (PPM)	Span Value (PPM)	Percent Of Span
Zero Gas	0				
Span					

O₂ Calibration:

Time (HRS)

***	Cylinder Value (%)	Analyzer Response (%)	Difference (%)	Span Value (%)	Percent Of Span
Zero Gas	0				
Mid Level					
High Level					

CO₂ Calibration:

Time: (HRS)

***	Cylinder Value (%)	Analyzer Response (%)	Difference (%)	Span Value (%)	Percent Of Span
Zero Gas	0				
Mid Level					
High Level					

Must be within 2% of the span for each calibration gas.

121593-GASTACKWPIFORMSS-420-14

INTERPOLL LABORATORIES, INC

(612) 786-6020

THC System Bias Check

Job _____ Source _____
 Test _____ Run _____ Date _____ Site _____
 Operator _____

Run	Time (HRS)	***	Cylinder Value (PPM)	Analyzer Resp (PPM)		Diff. CE-SB (PPM)	Span Val. (PPM)	% of Span
				Cal. Err.	Sys. Bias			
1		Zero Gas	0	0	1	1	100	1.0
		Upscale	30.3	30	30	0	100	0
2		Zero Gas	0	0	0	0	100	0
		Upscale	30.3	30	30	0	100	0
3	6712	Zero Gas	0	0	0	0	100	0
		Upscale	30.3	30	31	1	100	1.0
4	1355	Zero Gas	0	0	1	1	100	1.0
		Upscale	30.3	30	30	0	100	0
5	1534	Zero Gas	0	0	3	3	100	3
		Upscale	30.3	30	30	0	100	0
6	1718	Zero Gas	0	0	2	2	100	2.0
		Upscale	30.3	30			100	
7		Zero Gas	0					
		Upscale						
8		Zero Gas	0					
		Upscale						
9		Zero Gas	0					
		Upscale						
10		Zero Gas	0					
		Upscale						
11		Zero Gas	0					
		Upscale						
12		Zero Gas	0					
		Upscale						

Must be within 5% of the span for the zero or upscale cal. gas.

033194-GASTACKIWPFORMSS-420-11

INTERPOLL LABORATORIES, INC.
(612) 786-6020
EPA Method 2 Field Data Sheet

Drawing of Test Site

Job LP Hayward
 Source LINE 2 PRESS RTD Stack
 Test 14 Run Date
 Stack Dimen. IN.
 Dry Bulb °F Wet bulb °F
 Manometer ☐ Reg. ☐ Exp ☐ Elec.
 Barometric Pressure IN.HG
 Static Pressure IN.WC
 Operators
 Pitot No. C

Cross-section View	Elevation View
-----------------------	-------------------

Traverse Point No.	Fraction of Diameter	Distance From Stack Wall (IN.)	Distance From End of Port (IN.)	Velocity	Temp. of Gas (°F)
		Port Length: <u> </u> IN.	Time Start: <u> </u> HRS		
Temp. Meas. Device & S/N: <u> </u>				Time End: <u> </u> HRS	

R or nothing = reg. manometer; S = expanded; E = electronic

INTERPOL LABORATORIES, INC

(612) 786-6020

NOK System Bias Check

Job

LP / HAYWARD

Source

Line 2 Press RTO

Test

14 Run 1 -Date 6-8-84

Site

SMK IL

Operator

BOB

Run	Time (HRS)	***	Cylinder Value (PPM)	Analyzer Resp (PPM)		Diff. CE-SB (PPM)	Span Val. (PPM)	% of Span
				Cal. Err.	Sys. Bias			
1	1715	Zero Gas	0	0	1	1	500	.20
		Upscale	238	238	231	0	500	0
2	1854	Zero Gas	0	0	0	0	500	0
		Upscale	239	238	237	1	500	.20
3	0731	Zero Gas	0	0			500	
		Upscale	239	235	235	3	500	.60
4	1011	Zero Gas	0	0	0	0	250	0
		Upscale	239	235	238	0	250	0
5	1029	Zero Gas	0	0	0	0	100	0
		Upscale	78	76	78	2	100	2.0
6	1215	Zero Gas	0	0	0	0	100	0
		Upscale	78	76	78	2	100	2.0
7	1357	Zero Gas	0	0	1.0	1	100	1.0
		Upscale	78	76	79	3	100	3.0
8	1537	Zero Gas	0	0	4	4	100	4.0
		Upscale	78	76	74	2	100	2.0
9	1719	Zero Gas	0	0	0	0	100	0
		Upscale	78	76	73	3	100	3.0
10		Zero Gas	0					
		Upscale						
11		Zero Gas	0					
		Upscale						
12		Zero Gas	0					
		Upscale						

Must be within 5% of the span for the zero or upscale cal. gas.

033194-GASTACKIWP/FORMSS-420-11

INTERPOLL LABORATORIES, INC

(612) 786-6020

CO System Bias Check

Job

LPI HAYWARD

Source

Test

Run

Date

Site

Operator

Run	Time (HRS)	***	Cylinder Value (PPM)	Analyzer Resp (PPM)		Diff. CE-SB (PPM)	Span Val. (PPM)	% of Span
				Cal. Err.	Sys. Bias			
1	1715	Zero Gas	0	0	0	0	500	0
		Upscale	159	157	157	0	500	0
2	1854	Zero Gas	0	0	0	0	500	0
		Upscale	159	157	157	2	500	.40
3	0735	Zero Gas	0	0	5	5	500	1.00
		Upscale	159	157	158	1	500	.20
4	1011	Zero Gas	0	0	1	1	500	.20
		Upscale	159	157	155	2	500	.40
5	1215	Zero Gas	0	0	1	1	500	.20
		Upscale	159	157	154	3	500	.60
6	1351	Zero Gas	0	0	3	3	500	.60
		Upscale	159	157	155	2	500	.40
7	1537	Zero Gas	0	0	2	2	500	.40
		Upscale	159	157	154	3	500	.60
8	1719	Zero Gas	0	0	2	2	500	.40
		Upscale	159	157	153	4	500	.80
9		Zero Gas	0					
		Upscale						
10		Zero Gas	0					
		Upscale						
11		Zero Gas	0					
		Upscale						
12		Zero Gas	0					
		Upscale						

Must be within 5% of the span for the zero or upscale cal. gas.

033194-G:STACKWP\FORMS-420-11

INTERPOLL LABORATORIES, INC
(612) 786-6020
System Bias Check

Job LP1 HAYWARD Source _____
 Test _____ Run _____ Date _____ Site _____
 Operator _____

Run	Time (HRS)	***	Cylinder Value (PPM)	Analyzer Resp (PPM)		Diff. CE-SB (PPM)	Span Val. (PPM)	% of Span
				Cal. Err.	Sys. Bias			
1	1715	Zero Gas	0	0	0	0	25	0
		Upscale	13.5	13.4	13.5	.1	25	.40
2	1854	Zero Gas	0	0	0	0	25	0
		Upscale	13.5	13.4	13.3	-.1	25	.40
3	0735	Zero Gas	0	0	0	0	25	0
		Upscale	13.5	13.4	13.5	.1	25	.40
4	1014	Zero Gas	0	0	0	0	25	0
		Upscale	13.5	13.4	13.4	0	25	0
5	1215	Zero Gas	0	0	0	0	25	0
		Upscale	13.5	13.4	13.4	0	25	0
6	1357	Zero Gas	0	0	0	0	25	0
		Upscale	13.5	13.4	13.5	.1	25	.40
7	1537	Zero Gas	0	0	0	0	25	0
		Upscale	13.5	13.4	13.6	.2	25	.80
8	1719	Zero Gas	0	0	.1	-.1	25	.40
		Upscale	13.5	13.4	13.5	.1	25	.40
9		Zero Gas	0					
		Upscale						
10		Zero Gas	0					
		Upscale						
11		Zero Gas	0					
		Upscale						
12		Zero Gas	0					
		Upscale						

Must be within 5% of the span for the zero or upscale cal. gas.

INTERPOLL LABORATORIES, INC

(612) 786-6020

CO₂ System Bias Check

Job

LP/HAYWARD

Source

Test

Run

Date

Site

Operator

Run	Time (HRS)	***	Cylinder Value (PPM)	Analyzer Resp (PPM)		Diff. CE-SB (PPM)	Span Val. (PPM)	% of Span
				Cal. Err.	Sys. Bias			
1	1705	Zero Gas	0	0	0	0	20	0
		Upscale	11.1	11.0	11.1	.1	20	.50
2	1854	Zero Gas	0	0	0	0	20	0
		Upscale	11.1	11.0	11.1	.1	20	.50
3	0735	Zero Gas	0	0	.1	.1	20	.50
		Upscale	11.1	11.0	11.0	0	20	0
4	1011	Zero Gas	0	0	.2	.2	20	.10
		Upscale	11.1	11.0	11.0	0	20	0
5	1215	Zero Gas	0	0	.1	.1	20	.50
		Upscale	11.1	11.0	11.0	0	20	0
6	1351	Zero Gas	0	0	0	0	20	0
		Upscale	11.1	11.0	10.9	.1	20	.50
7	1537	Zero Gas	0	0	.1	.1	20	.50
		Upscale	11.1	11.0	11.0	0	20	0
8	1719	Zero Gas	0	0	0	0	20	0
		Upscale	11.1	11.0	10.9	.1	20	.50
9		Zero Gas	0					
		Upscale						
10		Zero Gas	0					
		Upscale						
11		Zero Gas	0					
		Upscale						
12		Zero Gas	0					
		Upscale						

Must be within 5% of the span for the zero or upscale cal. gas.

033194-GASTACKWPFORMS-420-11

INTERPOLL LABORATORIES

Calibration Error Check

Job W HaywardTest 14 Run _____ Date _____

Operator _____

CO

SO₂ Calibration:

Time (HRS) _____

***	Cylinder Value (ppm)	Analyzer Response (ppm)	Difference (ppm)	Span Value (ppm)	Percent of Span
Zero gas	0	0	0	500	0
Mid level	159	157	2	500	.40
High level	249	248		500	

NO_x Calibration:

Time (HRS) _____

***	Cylinder Value (ppm)	Analyzer Response (ppm)	Difference (ppm)	Span Value (ppm)	Percent of Span
Zero gas	0	0	0	500	0
Mid level	239	238	1	500	.20
High level	476	473	3	500	.60

O₂ Calibration:

Time (HRS) _____

***	Cylinder Value (ppm)	Analyzer Response (ppm)	Difference (ppm)	Span Value (ppm)	Percent of Span
Zero gas	0	0	0	25	0
Mid level	13.5	13.4	.1	25	.40
High level	21.0	20.8	.2	25	.80

CO₂ Calibration:

Time (HRS) _____

***	Cylinder Value (ppm)	Analyzer Response (ppm)	Difference (ppm)	Span Value (ppm)	Percent of Span
Zero gas	0	0	0	20	0
Mid level	11.1	11.0	.1	20	.50
High level	17.0	17.1	.1	20	.50

Must be within 2% of the span for each calibration gas

S-420-10

INTERPOLL LABORATORIES

Calibration Error Check

Job LP / HAYWARDTest 1 Run Date 6-7-94Operator BobSO₂ Calibration:Time (HRS)

***	Cylinder Value (ppm)	Analyzer Response (ppm)	Difference (ppm)	Span Value (ppm)	Percent of Span
Zero gas	0				
Mid level					
High level					

NO_x Calibration:Time (HRS) 0710

***	Cylinder Value (ppm)	Analyzer Response (ppm)	Difference (ppm)	Span Value (ppm)	Percent of Span
Zero gas	0	0	0	500	0
Mid level	239	239	0	500	0
High level	476	475	1	500	

O₂ Calibration:Time (HRS) 0710

***	Cylinder Value (ppm)	Analyzer Response (ppm)	Difference (ppm)	Span Value (ppm)	Percent of Span
Zero gas	0	0	0	25	0
Mid level	13.5	13.4	.1	25	.40
High level	21.0	21.0	0	25	0

CO₂ Calibration:Time (HRS) 0710

***	Cylinder Value (ppm)	Analyzer Response (ppm)	Difference (ppm)	Span Value (ppm)	Percent of Span
Zero gas	0	0	0	20	0
Mid level	11.1	11.0	.1	20	.50
High level	17.0	17.0	0	20	0

Must be within 2% of the span for each calibration gas

S-420-10

APPENDIX I

CALIBRATION GAS CERTIFICATION SHEETS

1890-1891

1891-1892

1892-1893

1893-1894

1894-1895

1895-1896

NATIONAL SPECIALTY GASES
630 UNITED DRIVE
DURHAM, N.C. 27713
(919) 544-3772

TO: TWIN CITY OXYGEN

CERTIFICATE OF ANALYSIS

DATE REPORTED: 12/17/93

REFERENCE #:88-28273

MATERIAL SUBMITTED: OXYGEN AND CARBON DIOXIDE IN NITROGEN,
CERTIFIED CYL. #CC92695

INFORMATION REQUESTED: RATIO ANALYSIS

METHOD OF ANALYSIS: OXYGEN AND INFRARED ANALYZERS

RESULT OF INVESTIGATION:

<u>COMPONENT</u>	<u>SPECIFICATION</u>	<u>CONCENTRATION</u>
O2	13.5%	13.5%
CO2	11%	11.1%
N2		BALANCE

Richard Sykes
AUTHORIZED SIGNATURE

THIS REPORT STATED ACCURATELY THE RESULTS OF THE INVESTIGATION MADE UPON THE MATERIAL SUBMITTED TO THE ANALYTICAL LABORATORY. EVERY EFFORT HAS BEEN MADE TO DETERMINE OBJECTIVELY, THE INFORMATION REQUESTED; HOWEVER, IN CONNECTION WITH ITS RENDERING OF THIS REPORT, NATIONAL SPECIALTY GASES SHALL HAVE NO LIABILITY IN EXCESS OF ITS ESTABLISHED CHARGE FOR THE SERVICE."

RECEIVED

DEC 29 1993

INTERPOLL LABORATORIES



Scott Specialty Gases, Inc.

1290 COMBERMERE STREET, TROY, MI 48063-0000
PHONE: 313-589-2950 FAX: 313-589-2134

9/02/91

GENEX
4018 DUNCAN AVENUE

PROJECT #: 05-26600
PO #: 4970SA

ST LOUIS

MO 63110-0000

CYLINDER #: ALM008828

ANALYTICAL ACCURACY: +-2%

COMPONENT	REQUESTED CONCENTRATION	ANALYSIS 1 (MOLES) U/M
CARBON MONOXIDE	150.0 PPM	150. PPM
NITROGEN	BALANCE	N/A

NOTES: CERTIFIED MASTER GAS

ANALYTICAL METHOD: CMG

DATE OF ANALYSIS: 7/29/91

ANALYST:

ANALYST

APPROVED BY:

SUPERVISOR



Scott Specialty Gases, Inc.

1290 COMBERMERE STREET, TROY, MI 48063-0000
PHONE: 313-589-2950 FAX: 313-589-2134

8/02/91

GENEX
4018 DUNCAN AVENUE

PROJECT #: 05-26600
PO #: 4970SA

ST LOUIS

MO 63110-0000

CYLINDER #: AAL19103

ANALYTICAL ACCURACY: +-2%

COMPONENT	REQUESTED CONCENTRATION	ANALYSIS 1 (MOLES) U/M
CARBON MONOXIDE	250.0 PPM	249. PPM
NITROGEN	BALANCE	N/A

NOTES: CERTIFIED MASTER GAS

ANALYTICAL METHOD: CMG

DATE OF ANALYSIS: 7/29/91

ANALYST

ANALYST

APPROVED BY:

SUPERVISOR

NATIONAL SPECIALTY GASES
630 UNITED DRIVE
DURHAM, NC 27713
(919)544-3772

CERTIFICATE OF ANALYSIS-EPA PROTOCOL MIXTURES

REFERENCE #: 88-29868 CYLINDER #:CC100138 CYL. PRESSURE:2000PSIG
EXPIRATION DATE:3/8/97 LAST ANALYSIS DATE:3/8/94
CUSTOMER:TWIN CITY OXYGEN P.O.# 9082

METHOD: ANALYZED ACCORDING TO EPA TRACEABILITY PROTOCOL FOR ASSAY AND CERTIFICATION
OF GASEOUS CALIBRATION STANDARDS-SEPTEMBER 1993-G-1

STANDARD: INSTRUMENT:BECKMAN THC
SRM #: 1667B MODEL #:400
CYL #: CLM5293 SERIAL #:1003052
CONC.: 47.3PPM LAST CAL:3/1/94

COMPONENT:PROPANE	COMPONENT:	COMPONENT:
MEAN CONC:30.3PPM	MEAN CONC:	MEAN CONC:
REPLICATE CONC.	REPLICATE CONC.	REPLICATE CONC.
DATE:3/8/94 DATE:	DATE: DATE:	DATE: DATE:
30.2PPM		
30.3PPM		
30.3PPM		

BALANCE GAS:AIR

REPLICATE DATA

DATE: 3/8/94					
Z	0	R	286.3	C	182.8
R	286.3	Z	0	C	183.4
Z	0	C	183.4	R	286.3

REPLICATE DATA

DATE:			
Z	R	C	
R	Z	C	
Z	C	R	

REPLICATE DATA

DATE:			
Z	R	C	
R	Z	C	
Z	C	R	

COMPONENT:PROPANE

DATE:			
Z	R	C	
R	Z	C	
Z	C	R	

COMPONENT:

DATE:			
Z	R	C	
R	Z	C	
Z	C	R	

COMPONENT:

DATE:			
Z	R	C	
R	Z	C	
Z	C	R	

Z=ZERO C=CANDIDATE R=REFERENCE

ANALYST:

Richard Sykes

APPROVED BY:

[Signature]

"THIS REPORT STATED ACCURATELY THE RESULTS OF THE INVESTIGATION MADE UPON THE MATERIAL SUBMITTED TO THE ANALYTICAL LABORATORY. EVERY EFFORT HAS BEEN MADE TO DETERMINE OBJECTIVELY, THE INFORMATION REQUESTED; HOWEVER, IN CONNECTION WITH ITS RENDERING OF THIS REPORT, NATIONAL SPECIALTY GASES SHALL HAVE NO LIABILITY IN EXCESS OF ITS ESTABLISHED CHARGE FOR THE SERVICE."

NATIONAL SPECIALTY GASES
330 UNITED DRIVE
DURHAM, NC 27713
(919)544-3772

CERTIFICATE OF ANALYSIS-EPA PROTOCOL MIXTURES

REFERENCE #: 88-29870 CYLINDER #:CC98059 CYL. PRESSURE:2000PSIG
EXPIRATION DATE:3/8/97 LAST ANALYSIS DATE:3/8/94
CUSTOMER:TWIN CITY OXYGEN P.O.# 9082

METHOD: ANALYZED ACCORDING TO EPA TRACEABILITY PROTOCOL FOR ASSAY AND CERTIFICATION
OF GASEOUS CALIBRATION STANDARDS-SEPTEMBER 1993:G-1

STANDARD: INSTRUMENT:BECKMAN THC
SRM #: 1669B MODEL #:400
CYL #: CLM789 SERIAL #:1003052
CONC.: 464PPM LAST CAL:3/1/94

COMPONENT:PROPANE
MEAN CONC:303PPM
REPLICATE CONC.
DATE:3/8/94 DATE:
303PPM
303PPM
304PPM

COMPONENT:
MEAN CONC:
REPLICATE CONC.
DATE: DATE:

COMPONENT:
MEAN CONC:
REPLICATE CONC.
DATE: DATE:

BALANCE GAS:AIR

REPLICATE DATA

DATE: 3/8/94
Z 0 R 321.2 C 209.7
R 321.1 Z 0 C 209.7
Z 0 C 210.4 R 321.2

REPLICATE DATA

DATE:
Z R C
R Z C
Z C R

REPLICATE DATA

DATE:
Z R C
R Z C
Z C R

COMPONENT:PROPANE

DATE:
Z R C
R Z C
Z C R

COMPONENT:

DATE:
Z R C
R Z C
Z C R

COMPONENT:

DATE:
Z R C
R Z C
Z C R

Z=ZERO C=CANDIDATE R=REFERENCE

ANALYST: Richard Sykes

APPROVED BY: 

THIS REPORT STATED ACCURATELY THE RESULTS OF THE INVESTIGATION MADE UPON THE MATERIAL SUBMITTED TO THE ANALYTICAL LABORATORY. EVERY EFFORT
HAS BEEN MADE TO DETERMINE OBJECTIVELY, THE INFORMATION REQUESTED; HOWEVER, IN CONNECTION WITH ITS RENDERING OF THIS REPORT, NATIONAL
SPECIALTY GASES SHALL HAVE NO LIABILITY IN EXCESS OF ITS ESTABLISHED CHARGE FOR THE SERVICE.

Interpoll Laboratories, Inc.
(612) 786-6020

CERTIFICATE OF ANALYSIS FOR
NO STANDARD GASES FOR METHOD 7E

Vendor: Scott Specialty Gases
Cylinder No: ALMO00157
Date of Preparation: 7-21-91
Label: 78.7 ppm NOx
Blend Specification: _____

Results Of Analyses Of Standard Gas (by Method 7A)

Date of Analysis	Run	NO in N ₂ (ppm)
<u>8-10-93</u>	<u>1</u>	<u>78.68</u>
<u>"</u>	<u>2</u>	<u>78.14</u>
<u>"</u>	<u>3</u>	<u>78.03</u>
<u> </u>	<u>4</u>	<u> </u>
<u> </u>	<u>5</u>	<u> </u>
<u> </u>	<u>6</u>	<u> </u>
	Avg	<u>78.28</u>

Analyst: Bob Aschenbach

- ☒ Results are within 10% of the vendor tag value; use tag value.
☐ Results are not within 10% of the vendor tag value; conduct another set of triplicate analyses.
☐ Results of six consecutive analyses within $\pm 10\%$ of the average; relabel as above.
☐ All results not within $\pm 10\%$ of the average; perform another set of triplicate analyses.

Approved by,

August 16, 1993
Date

Dennis J. Perry
Dr. Perry Lannes

Interpoll Laboratories, Inc.
(612) 786-6020

Printout of ESC Model 80 DAS
for CEM Trailer No. 1
- 1993 -

File Name: CG10
Job Number: 3-3333
Client: Interpoll Laboratories Inc
Location: Circle Pines, Minnesota

ALM000157 - 78.7 ppm NOx -- Run 1 - 3

Julian	Time	
Conc. (dry basis unless noted)		
Date	(Hrs)	NOx (ppmv)
222	13:52:00	79.0
222	13:52:30	78.7
222	13:53:00	78.7
222	13:53:30	78.4
222	13:54:00	157
222	13:54:30	226
222	13:55:00	232
222	13:55:30	233
222	13:56:00	5.
222	13:56:30	1.6
222	13:57:00	26.5
222	13:57:30	77.8
222	13:58:00	78.2
222	13:58:30	78.2
222	13:59:00	78.1
222	13:59:30	78.3
222	14:00:00	78.1
222	14:00:30	78.1
222	14:01:00	27.4
222	14:01:30	1.0
222	14:02:00	148
222	14:02:30	227
222	14:03:00	232
222	14:03:30	232
222	14:04:00	80.1
222	14:04:30	78.2
222	14:05:00	78.2
222	14:05:30	78.0
222	14:06:00	78.1
222	14:06:30	77.8



Scott Specialty Gases, Inc.

1290 COMBERMERE STREET, TROY, MI 48063-0000
PHONE: 313-589-2950 FAX: 313-589-2134

8/02/91

GENEX
4018 DUNCAN AVENUE

PROJECT #: 05-26600
PO #: 4970SA

ST LOUIS

MO 63110-0000

CYLINDER #: ALM000157

ANALYTICAL ACCURACY: +-2%

COMPONENT	REQUESTED CONCENTRATION	ANALYSIS 1 (MOLES) U/M
NITRIC OXIDE	80.0 PPM	78.2 PPM
NITROGEN - OXYGEN FREE	BALANCE	N/A

NOTES: CERTIFIED MASTER GAS
NOX=78.7 PPM NITROGEN DIOXIDE=0.5 PPM

ANALYTICAL METHOD: CMG

DATE OF ANALYSIS: 7/25/91

ANALYST:

ANALYST

APPROVED BY:

SUPERVISOR

Interpoll Laboratories, Inc.
(612) 786-6020

CERTIFICATE OF ANALYSIS FOR
NO STANDARD GASES FOR METHOD 7E

Vendor: National Specialty Gases
Cylinder No: CC114192
Date of Preparation: 3-23-93
Label: 239 ppm NOx
Blend Specification: _____

Results Of Analyses Of Standard Gas (by Method 7A)

Date of Analysis	Run	NO in N ₂ (ppm)
<u>8-10-93</u>	<u>1</u>	<u>239.500</u>
<u>"</u>	<u>2</u>	<u>239.200</u>
<u>"</u>	<u>3</u>	<u>239.00</u>
<u> </u>	<u>4</u>	<u> </u>
<u> </u>	<u>5</u>	<u> </u>
<u> </u>	<u>6</u>	<u> </u>
<u> </u>	<u>Avg</u>	<u>239.2</u>

Analyst: Bob Aschenbach

- ☒ Results are within 10% of the vendor tag value; use tag value.
☐ Results are not within 10% of the vendor tag value; conduct another set of triplicate analyses.
☐ Results of six consecutive analyses within $\pm 10\%$ of the average; relabel as above.
☐ All results not within $\pm 10\%$ of the average; perform another set of triplicate analyses.

Approved by,

August 16, 1993
Date

Dennis H. Perry
Dr. Perry Lannes

Interpoll Laboratories, Inc.
(612) 786-6020

Printout of ESC Model 80 DAS
for CEM Trailer No. 1
- 1993 -

File Name: CG3
Job Number: 3-3333
Client: Interpoll Laboratories
Location: Circle Pines, Minnesota

CC114192 - 239 ppm NOx -- Run 1 - 3

Julian

Time

%. (dry basis unless noted)

Date	(Hrs)	NOx (ppmv)
222	10:22:00	240
222	10:22:30	240
222	10:23:00	239
222	10:23:30	239
222	10:24:00	234
222	10:24:30	233
222	10:25:00	233
222	10:25:30	216
222	10:26:00	239
222	10:26:30	239
222	10:27:00	240
222	10:27:30	240
222	10:28:00	239
222	10:28:30	239
222	10:29:00	237
222	10:29:30	232
222	10:30:00	232
222	10:30:30	233
222	10:31:00	230
222	10:31:30	239
222	10:32:00	239
222	10:32:30	239
222	10:33:00	239
222	10:33:30	239
222	10:34:00	239
222	10:34:30	239

Run 1 <

Run 2 <

Run 3 <

NATIONAL SPECIALTY GASES
630 UNITED DRIVE
DURHAM, NC 27713
(919) 544-3772

CERTIFICATE OF ANALYSIS-EPA PROTOCOL MIXTURES

REFERENCE #: 88-23182 CYLINDER #: CC114192 CYL PRESSURE: 2000PSIG

EXPIRATION DATE: 3-23-95

LAST ANALYSIS DATE: 3-23-93

CUSTOMER: TWIN CITY OXYGEN

P.O.#

METHOD: EPA PROTOCOL # 1 3.0.4. G-1

STANDARD:

SRM #: 1685B

CYL #: CLM-4728

CONC.: 248 PPM

INSTRUMENT:

COMPONENT: BECKMAN
CHEMILUMINESCENT

MODEL #: 951A

SERIAL #: 100532

LAST CAL: 1-2-93

COMP: NO
MEAN CONC: 239 PPM

REPLICATE CONC.

DATE: 3-16-93	DATE: 3-23-93
240 PPM	236 PPM
240 PPM	237 PPM
241 PPM	238 PPM

COMP: NO2
MEAN CONC: 2.99 PPM

REPLICATE CONC.

DATE: DATE:

COMP:
MEAN CONC:

REPLICATE CONC.

DATE: DATE:

BALANCE GAS: NITROGEN

APPENDIX J

PROCESS RATE INFORMATION

71-34-3454

TO INTERPOLL LABORATORIES, INC
CIRCLE PINES, MN 55014-1819

LETTER OF TRANSMITTAL

[illegible]

WE ARE SENDING YOU

☒ Attached ☐ Under separate cover via _____ the following items:

☐ Shop Drwgs. ☐ Prints ☐ Plans ☐ Samples ☐ Specifications☐ Copy of Letter ☐ Change Order ☐ _____[illegible]

THESE ARE TRANSMITTED as checked below:

☐ For Approval☐ Approved As Submitted

☐ Submit _____ copies for distribution

x For Your Use

☐ Approved As Noted☐ Return corrected prints☒ As Requested☐ Returned For Corrections

☐ _____

☐ For Review & Comment☐ Resubmit _____ copies for approval

☐ _____

☐ FOR BIDS DUE _____ 199.

REMARKS

[illegible]

Copy To: File, Jim Ross DNR, Brad Pyle DNR

Signed: Sue Somers

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Hayward Press and Thermal Oil Heater testing June 7-10, 1994
TEST SCHEDULE LINE 1

LINE 1 PRESS TESTING JUNE 7, 1994 - FORMALDEHYDE

<u>DATE</u>	<u>POLLUTANT</u>	<u>RUN #1</u>	<u>RUN #2</u>	<u>RUN #3</u>
6-7	HCHO	1250-1352	1420-1522	1545-1647

LINE 1 PRESS TESTING JUNE 8, 1994 - MDI

<u>DATE</u>	<u>POLLUTANT</u>	<u>RUN #1</u>	<u>RUN #2</u>	<u>RUN #3</u>
6-7	MDI	0815-0916	0945-1046	1115-1216

LINE 1 THERMAL OIL HEATER JUNE 8, - TSP, CO, NOX

<u>DATE</u>	<u>POLLUTANT</u>	<u>RUN #1</u>	<u>RUN #2</u>	<u>RUN #3</u>
6-8	TSP	1538-1640	1708-1811	1835-1938
6-8	CO	1538-1640	1708-1811	1835-1938
6-8	NOX	1538-1640	1708-1811	1835-1938

LINE 1 THERMAL OIL HEATER - JUNE 9, - POM, PHENOL, BENZENE, FORMALDEHYDE

<u>DATE</u>	<u>POLLUTANT</u>	<u>RUN #1</u>	<u>RUN #2</u>	<u>RUN #3</u>
6-9	POM	0851-1052	1240-1430 1522-1534	1610-1812
6-9	PHENOL	0845-0945	1000-1100	1111-1130 1236-1320
6-9	BENZENE	0845-0945	1000-1100	1111-1130 1236-1320
6-9	FORMALDEHYDE	1345-1415 1535-1606	1632-1743	1802-1904

LINE 1 PRESS TESTING JUNE 10, 1994 - TSP, VOC, CO, NOX

<u>DATE</u>	<u>POLLUTANT</u>	<u>RUN #1</u>	<u>RUN #2</u>	<u>RUN #3</u>
6-10	TSP	0935-1036	1100-1205	1220-1322
	VOC	0935-1036	1100-1205	1220-1322
	CO	0935-1036	1100-1205	1220-1322
	NOX	0935-1036	1100-1205	1220-1322

Hayward Press and Thermal Oil Heater testing June 7-10, 1994
TEST SCHEDULE LINE 2

LINE 2 THERMAL OIL HEATER JUNE 7. - POM, BENZENE

<u>DATE</u>	<u>POLLUTANT</u>	<u>RUN #1</u>	<u>RUN #2</u>	<u>RUN #3</u>
6-7	POM	0827-1036	1136-1342	1425-1627
6-7	BENZENE	0849-0951	1142-1242	1436-1536

LINE 2 THERMAL OIL HEATER - JUNE 8. - PHENOL, FORMALDEHYDE, PM, CO, NOx

6-8	PM	0757-0858	0920-1021	1114-1215
6-8	CO	0757-0858	0920-1021	1114-1215
6-8	NOX	0757-0858	0920-1021	1114-1215
6-8	HCHO	1446-1553	1616-1718	1742-1843
6-8	PHENOL	1446-1553	1616-1718	1742-1843

LINE 2 PRESS TESTING JUNE 9, 1994 - MDI, PM, VOC, CO, NOX

<u>DATE</u>	<u>POLLUTANT</u>	<u>RUN #1</u>	<u>RUN #2</u>	<u>RUN #3</u>
6-9	PM	1240-1342	1425-1527	1605-1719
6-9	VOC	1240-1342	1425-1527	1605-1719
6-9	CO	1240-1342	1425-1527	1605-1719
6-9	NOX	1240-1342	1425-1527	1605-1719
6-9	MDI	1325-1441	1518-1641	1712-1828

LINE 2 PRESS TESTING JUNE 10, 1994 - FORMALDEHYDE

<u>DATE</u>	<u>POLLUTANT</u>	<u>RUN #1</u>	<u>RUN #2</u>	<u>RUN #3</u>
6-10	HCHO	0815-0918	0941-1043	1121-1200 1315-1333

LINE 1 PRESS TESTING JUNE 7, 1994 - FORMALDEHYDE

19.64 =Plant Production rate in Tons per hour
356 =MDI resin usage in pounds per hour
0.91% =MDI resin usage as % of finished product
856 =Liquid phenolic resin usage in pounds per hour (100% solids)
2.18% =Liquid phenolic resin usage as % of finished product (100% solids)
334 =Wax usage in pounds per hour
0.85% =Wax usage as % of finished product

LINE 1 PRESS TESTING JUNE 8, 1994 - MDI

19.83 =Plant Production rate in Tons per hour
392 =MDI resin usage in pounds per hour
0.99% =MDI resin usage as % of finished product
905 =Liquid phenolic resin usage in pounds per hour (100% solids)
2.28% =Liquid phenolic resin usage as % of finished product (100% solids)
318 =Wax usage in pounds per hour
0.80% =Wax usage as % of finished product

LINE 1 PRESS TESTING JUNE 10, 1994 - TSP, VOC, CO, NOX

18.93 =Plant Production rate in Tons per hour
341 =MDI resin usage in pounds per hour
0.90% =MDI resin usage as % of finished product
816 =Liquid phenolic resin usage in pounds per hour (100% solids)
2.16% =Liquid phenolic resin usage as % of finished product (100% solids)
331 =Wax usage in pounds per hour
0.87% =Wax usage as % of finished product

LINE 1 THERMAL OIL HEATER JUNE 8, - TSP, CO, NOX

20.46 =Production rate in Tons per hour
0.35 =K1 estimated Tons per hour of fuel burned based on fuel measurement
6.24 =K1 estimated mmBTU per hour input based on fuel measurement
0.39 =K2 estimated Tons per hour of fuel burned based on fuel measurement
7.03 =K2 estimated mmBTU per hour input based on fuel measurement
0.74 =Total tons of dry bark per hour input
13.27 =Total mmBTU per hour input

LINE 1 THERMAL OIL HEATER - JUNE 9, - POM

20.01 =Production rate in Tons per hour
0.31 =K1 estimated Tons per hour of fuel burned based on fuel measurement
5.58 =K1 estimated mmBTU per hour input based on fuel measurement
0.31 =K2 estimated Tons per hour of fuel burned based on fuel measurement
5.54 =K2 estimated mmBTU per hour input based on fuel measurement
0.62 =Total tons of dry bark per hour input
11.12 =Total mmBTU per hour input

LINE 1 THERMAL OIL HEATER - JUNE 9, - PHENOL, BENZENE

19.86 =Production rate in Tons per hour
0.27 =K1 estimated Tons per hour of fuel burned based on fuel measurement
4.78 =K1 estimated mmBTU per hour input based on fuel measurement
0.25 =K2 estimated Tons per hour of fuel burned based on fuel measurement
4.50 =K2 estimated mmBTU per hour input based on fuel measurement
0.52 =Total tons of dry bark per hour input
9.28 =Total mmBTU per hour input

LINE 1 TCH JUN 9 - FORMALDEHYDE

0.57 = TOTAL TONS
10.31 mm BTU

LINE 2 THERMAL OIL HEATER JUNE 7, - POM

17.63 =Production rate in Tons per hour
0.83 =K3 estimated Tons per hour of fuel burned based on fuel measurement
14.92 =K3 estimated mmBTU per hour input based on fuel measurement
0.20 =K4 estimated Tons per hour of fuel burned based on fuel measurement
3.66 =K4 estimated mmBTU per hour input based on fuel measurement
1.03 =Total tons of dry bark per hour input
18.58 =Total mmBTU per hour input

LINE 2 THERMAL OIL HEATER JUNE 7, BENZENE

20.40 =Production rate in Tons per hour
0.78 =K3 estimated Tons per hour of fuel burned based on fuel measurement
13.97 =K3 estimated mmBTU per hour input based on fuel measurement
0.20 =K4 estimated Tons per hour of fuel burned based on fuel measurement
3.55 =K4 estimated mmBTU per hour input based on fuel measurement
0.98 =Total tons of dry bark per hour input
17.52 =Total mmBTU per hour input

LINE 2 THERMAL OIL HEATER JUNE 8, - TSP, CO, NOX

19.23 =Production rate in Tons per hour
0.56 =K3 estimated Tons per hour of fuel burned based on fuel measurement
10.01 =K3 estimated mmBTU per hour input based on fuel measurement
0.14 =K4 estimated Tons per hour of fuel burned based on fuel measurement
2.46 =K4 estimated mmBTU per hour input based on fuel measurement
0.70 =Total tons of dry bark per hour input
12.47 =Total mmBTU per hour input

LINE 2 THERMAL OIL HEATER - JUNE 8, - PHENOL, FORMALDEHYDE

17.16 =Production rate in Tons per hour
0.45 =K3 estimated Tons per hour of fuel burned based on fuel measurement
8.02 =K3 estimated mmBTU per hour input based on fuel measurement
0.06 =K4 estimated Tons per hour of fuel burned based on fuel measurement
1.05 =K4 estimated mmBTU per hour input based on fuel measurement
0.51 =Total tons of dry bark per hour input
9.07 =Total mmBTU per hour input

LINE 2 PRESS TESTING JUNE 9, 1994 - PM, VOC, CO, NOX

19.04 =Plant Production rate in Tons per hour
316 =MDI resin usage in pounds per hour
0.83% =MDI resin usage as % of finished product
729 =Liquid phenolic resin usage in pounds per hour (100% solids)
1.92% =Liquid phenolic resin usage as % of finished product (100% solids)
308 =Wax usage in pounds per hour
0.81% =Wax usage as % of finished product

LINE 2 PRESS TESTING JUNE 9, 1994 - MDI

19.00 =Plant Production rate in Tons per hour
326 =MDI resin usage in pounds per hour
0.86% =MDI resin usage as % of finished product
719 =Liquid phenolic resin usage in pounds per hour (100% solids)
1.89% =Liquid phenolic resin usage as % of finished product (100% solids)
348 =Wax usage in pounds per hour
0.92% =Wax usage as % of finished product

LINE 2 PRESS TESTING JUNE 10, 1994 - FORMALDEHYDE

19.09 =Plant Production rate in Tons per hour
305 =MDI resin usage in pounds per hour
0.80% =MDI resin usage as % of finished product
671 =Liquid phenolic resin usage in pounds per hour (100% solids)
1.76% =Liquid phenolic resin usage as % of finished product (100% solids)
255 =Wax usage in pounds per hour
0.67% =Wax usage as % of finished product

LINE 1 PRESS TESTING JUNE 7, 1994 - FORMALDEHYDE

DATA TIME: START= 12:40 END= 17:00 HOURS= 4.33

BOARD WEIGHTS - LBS

Weights of approximately every 25th untrimmed board (from press tapes)
7/16"

196	197	184	190
193	194	186	195
196	193	188	193
196	191	188	194
195	191	184	193
195	185	191	196
193	186	186	192
194	189	187	195
195	189	190	196
193	186	189	194

191.45 lb=average
untrimmed
mat weight

179.58 lb=average
finished board
weight
(untrimmed mat
weight-weight
of trim)

6.2% =trim %

$$\frac{948 \times 8 \times 16}{4.33} = 28.024 \frac{\text{mat}}{\text{hr}} \quad 7/16$$

PLANT PRODUCTION RATE

4.33 =hours during testing

79 =pressloads

948 =no. of 8'x16' boards produced (pressloads x12 boards per load)

170242 =lbs of finished product (boards produced x weight of finished board)

39287 =lbs of finished product per hour (lbs of finished product / hours)

19.64 =tons of finished product per hour (lbs of finished product per hour / 2000 lb)

RESIN USAGE FROM TANK MEASUREMENTS

Note: common tanks supply wax and resin to both Line 1 and Line 2. Usage for one line is estimated by proportioning the total usage by the footage (3/8" basis) for each line)

MEASUREMENT SUMMARY:

				PHENOLIC	PHENOLIC	WAX	WAX
				61%	100%	58%	100%
				solids	solids	solids	solids
time	line 1 footage	line 2 footage	MDI lbs	lbs	lbs	lbs	lbs
13:00	34049	32257	894	3474	2119	763	465
14:00	34049	0	149	880	537	764	466
15:00	32257	17921	447	1931	1178	764	466
16:00	35841	32257	893	2497	1523	764	466
17:00	34049	32257	596	2958	1804	1527	931
hourly average	34049	22938.4	595.8	2348	1432	916.4	559
Line 1			356		856		334
Line 2			240		577		225

39287 =average lbs. per hour finished product produced during testing

356 =average lbs. per hour of MDI resin used during testing

0.91% = MDI resin used as % of finished product

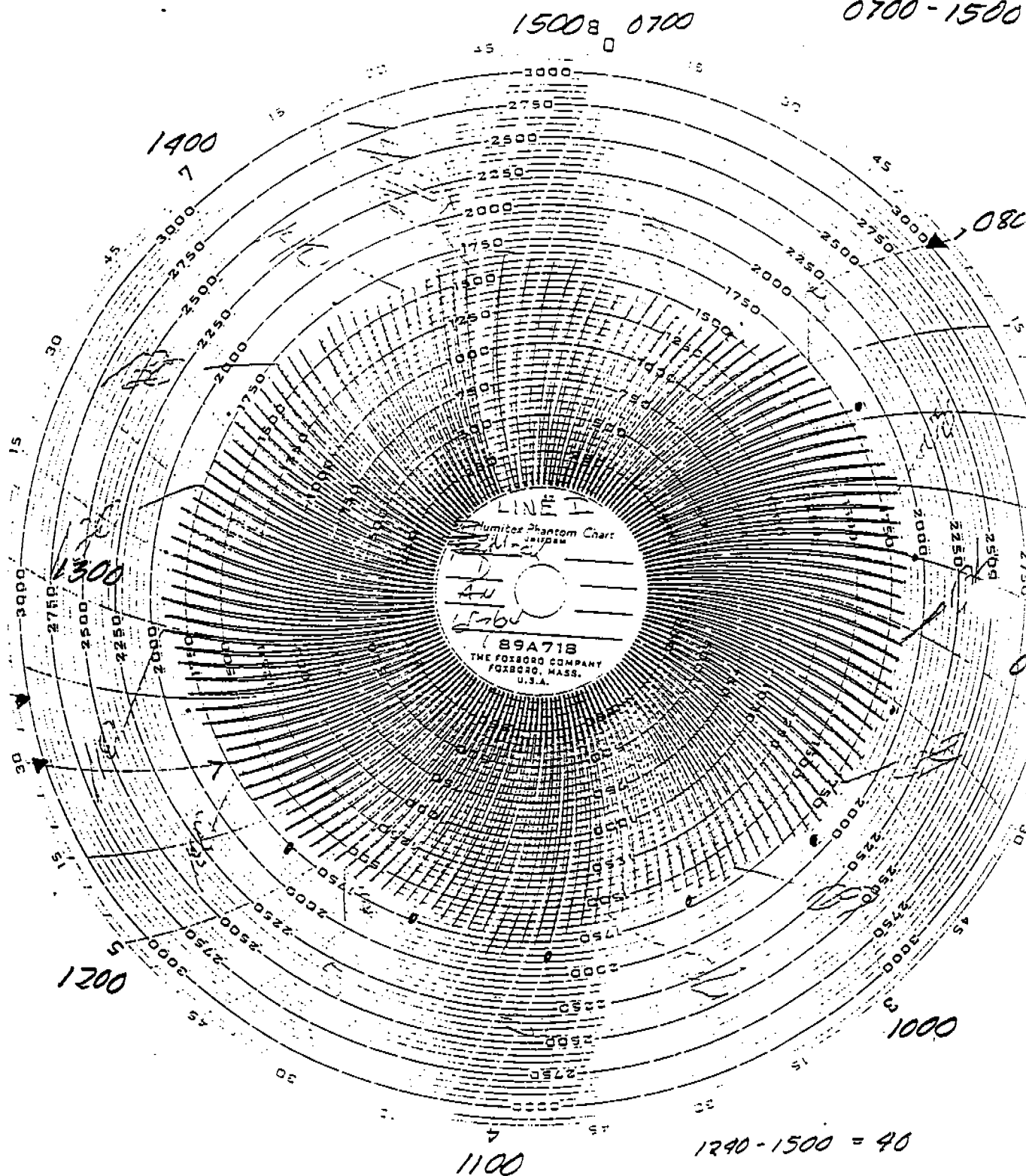
856 =average lbs. per hour of phenolic resin (100% solids) used during testing

2.18% =Phenolic resin used as % of finished product

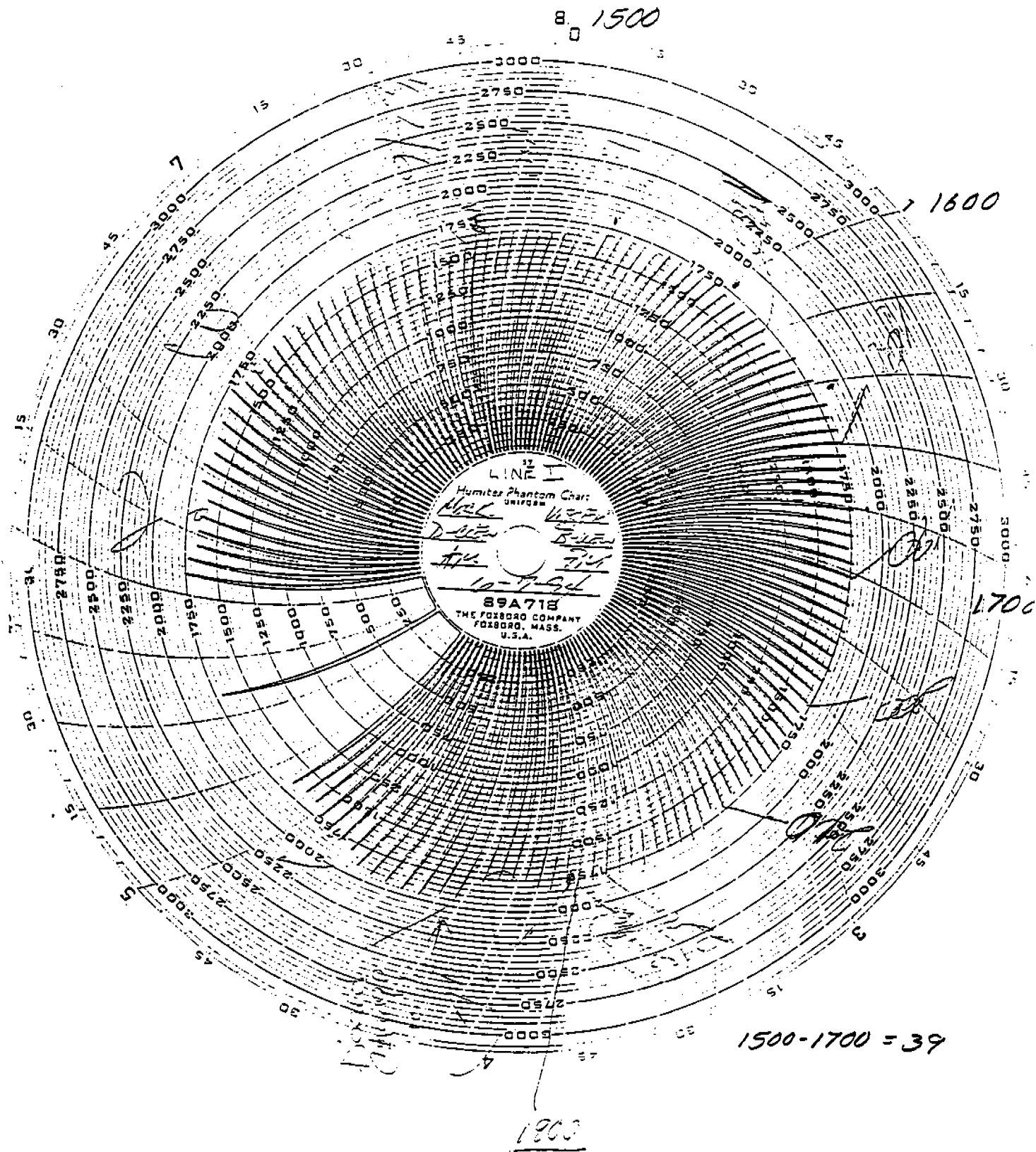
334 =average lbs. per hour of wax (100% solids) used during testing

0.85% =wax used as % of finished product

LINE I
PRESS CHART
6-7-99
0700-1500



LINE I
PRESS CHART
6-7-94
1500 - 2300



PRESS REPORT - LINE 1

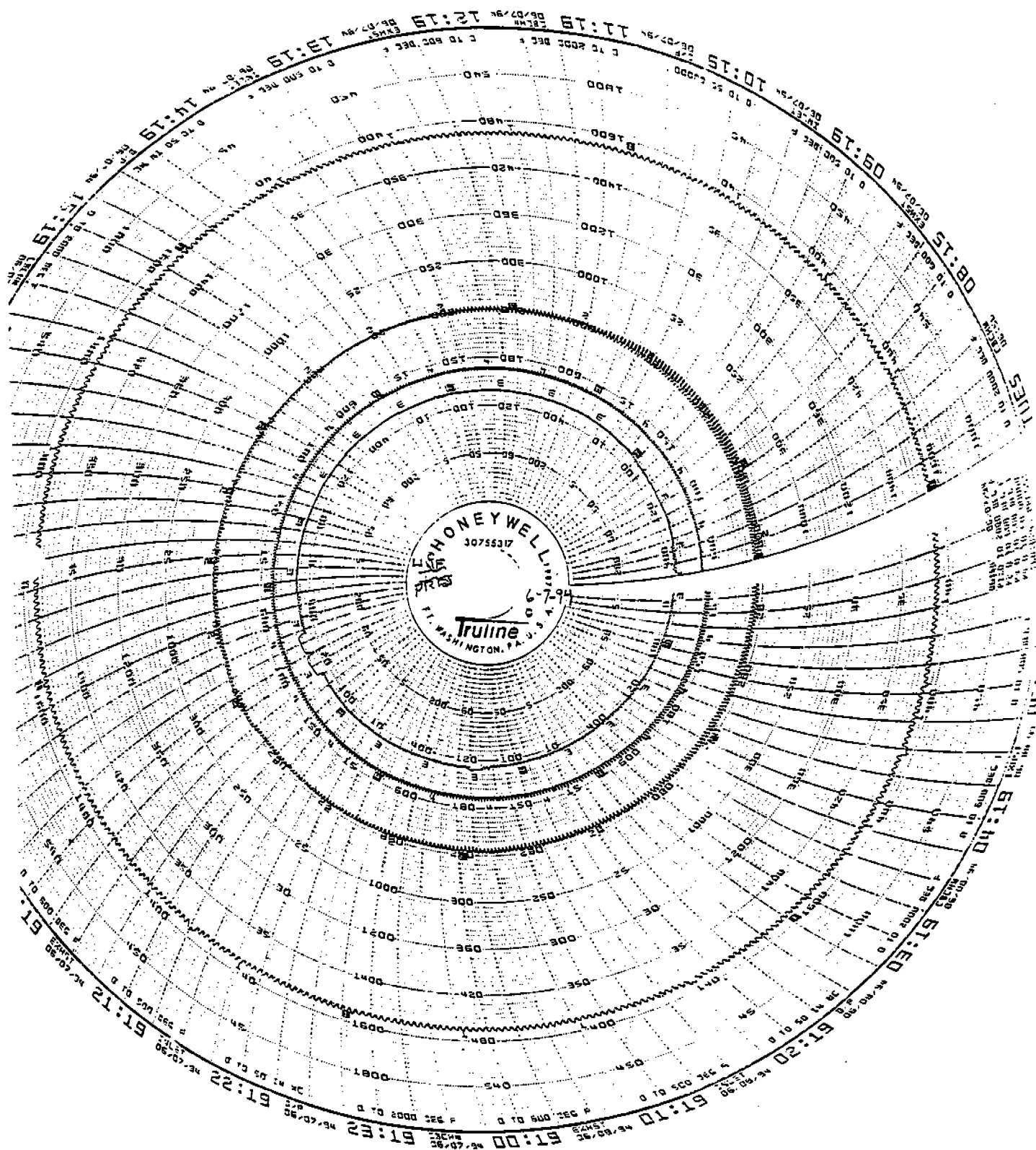
LINE SPEED	FROM	TO
30	700	
40 50	700	7:30
60	8:00	
65	12:30	
66	1:30	

PRESS LOADS 228 1/16
 DEPRESSION TIME 2055
 TOTAL RESULTS:
 LOG COUNT: 8054
 F.C.O.S. EYE RADIATOR YES
 Cleaned Blender Sumpkins & Tracks YES
 Cleaned Ductile Coating YES
 Press Blown Down YES
 Hardware Cleaned YES/NO
 How Many 0
 Former Eye Radiator YES

[illegible]

E - Electrical C - Counter

LINE I
PRESS RTO
CHART
6-7-99



10

L-T PRESS B-7-94

108 2

RECOVERED

#1	#2	#3	#4	#5	INLET PRESS.	BURNERS B #1	BURNERS B #2	INLET TEMP.	COMBUST. CHAMBER TEMP.	EXHAUST TEMP.	AMP.	GAS
8.0	436	484	407	438	36 w.c.	1612	1606	108	1535	230	13.6	017346
8.5	435	484	405	435	37 w.c.	1586	1603	109	1540	232	13.7	017348
8.30	434	484	409	394	38 w.c.	1618	1588	110	1565	239	13.6	017350
8.45	431	485	405	441	37 w.c.	1598	1610	108	1545	232	13.6	017362
9.2	435	480	409	389	37 w.c.	1609	1581	109	1552	244	13.9	017354
9.15	436	480	404	442	37 w.c.	1588	1606	109	1538	232	13.7	017356
9.20	438	477	409	386	38 w.c.	1617	1592	109	1554	241	13.8	017358
9.45	438	479	403	433	38 w.c.	1583	1604	109	1537	234	13.8	017360
10.2	439	478	405	406	36 w.c.	1585	1592	110	1536	243	13.8	017362
10.10	441	478	407	390	37 w.c.	1602	1579	112	1545	248	13.8	017365
10.20	439	479	406	415	36 w.c.	1593	1612	112	1542	235	13.6	017367
10.45	441	480	406	446	36 w.c.	1594	1610	114	1542	235	13.7	017369
11.0	441	478	411	405	40 w.c.	1612	1587	112	1550	244	13.8	017371
11.15	436	480	421	409	39 w.c.	1612	1583	114	1554	244	13.9	017373
11.20	430	483	430	424	37 w.c.	1668	1585	114	1536	242	13.9	017375
11.45	435	484	439	468	38 w.c.	1599	1609	113	1546	236	13.6	017377
12.1	433	486	441	471	37 w.c.	1583	1603	114	1537	237	13.9	017379
12.15	430	487	447	445	37 w.c.	1582	1593	112	1537	239	13.8	017381
12.30	432	486	454	437	37 w.c.	1620	1603	114	1554	242	13.9	017383
12.45	428	486	454	452	36 w.c.	1578	1592	113	1533	239	13.8	017385
1.0	426	490	459	471	37 w.c.	1609	1616	114	1549	237	13.6	017387
1.15	423	490	464	436	37 w.c.	1620	1597	114	1555	244	13.9	017389
1.30	420	493	461	462	36 w.c.	1578	1597	113	1536	240	13.9	017391
1.45	416	491	467	452	3.8 w.c.	1619	1592	114	1554	243	14.0	017393
2.0	414	487	463	434	3.9 w.c.	1591	1585	115	1542	239	13.8	017395
2.15	418	482	462	462	3.8 w.c.	1617	1613	113	1553	240	13.9	017397

LINE 1 PRESS TESTING JUNE 8, 1994 - MDI

DATA TIME START= 08:00 END= 12:30 HOURS= 4.50

BOARD WEIGHTS - LBSweights of approximately every 25th untrimmed board (from press tapes)
7/16"

191	186	196	190	191.08 lb=average
191	192	194	192	untrimmed
187	193	193	190	mat weight
191	193	197	186	
195	192	194	190	179.23 lb=average
191	185	193	191	finished board
188	187	197	188	weight
186	187	193	189	(untrimmed mat
188	191	194	198	weight-weight
183	194	192		of trim)

6.2% =trim %

PLANT PRODUCTION RATE

4.50 =hours during testing

83 =pressloads

996 =no. of 8'x16' boards produced (pressloads x12 boards per load)

178513 =lbs of finished product (boards produced x weight of finished board)

39670 =lbs of finished product per hour (lbs of finished product / hours)

19.83 =tons of finished product per hour (lbs of finished product per hour / 2000 lb)

*28.33 msl / hr 7/16*RESIN USAGE FROM TANK MEASUREMENTS

Note: common tanks supply wax and resin to both Line 1 and Line 2. Usage for one line is estimated by proportioning the total usage by the footage (3/8" basis) for each line)

MEASUREMENT SUMMARY:

	line 1 footage	line 2 footage	MDI lbs	PHENOLIC 61% solids	PHENOLIC 100% solids	WAX 58% solids	WAX 100% solids
				lbs	lbs	lbs	lbs
09:00	34049	34049	596	2649	1616	1145	664
10:00	34049	32257	1192	2507	1529	764	443
11:00	35841	30465	298	2362	1441	382	222
12:00	28673	34049	894	2467	1505	1146	665
13:00	34049	32257	297	2436	1486	1145	664
hourly							
average	33332	32615	655	2484	1515	916	532
Line 1			392		905		318
Line 2			264		610		214

39670 =average lbs. per hour finished product produced during testing

392 =average lbs. per hour of MDI resin used during testing

0.99% = MDI resin used as % of finished product

905 =average lbs. per hour of phenolic resin (100% solids) used during testing

2.28% =Phenolic resin used as % of finished product

318 =average lbs. per hour of wax (100% solids) used during testing

0.80% =wax used as % of finished product

BOARD WEIGHTS - LBS

Weights of approximately every 25th untrimmed board (from press tapes)
16 and 1/2"

191	191	194	191
188	190	199	191
187	193	198	186
184	200	198	192
184	189	192	190
189	196	191	186
185	197	192	187
186	200	195	188
187	199	193	187
194	201	196	

191.72 lb=average
untrimmed
mat weight

179.83 lb=average
finished board
weight
(untrimmed mat
weight-weight
of trim)

6.2% =trim %

PLANT PRODUCTION RATE

4.17 =hours during testing

79 =pressloads

948 =no. of 8'x16' boards produced (pressloads x 2 boards per load)

170479 =lbs of finished product (boards produced x weight of finished board)

40915 =lbs of finished product per hour (lbs of finished product / hours)

20.46 =tons of finished product per hour (lbs of finished product per hour / 2000 lb)

$$\frac{948 \times 8 \times 16}{4.17} = 29.1 \text{ mst/hr } 7/10$$

EL BURNING RATE ESTIMATED BY BARK INPUTK1

10 =K1 fuel calibration in pounds per count

479 =K1 counts during testing hours

4790 =K1 lbs of wet fuel burned during testing

4.17 =hours during testing

39.7% =average moisture content of fuel

2888 =total pounds of dry fuel burned during testing (wet pounds x (1- moisture content))

693 =lbs of dry fuel burned per hour during testing (pounds of dry fuel / testing hours)

0.35 =tons of dry fuel burned per hour during testing (pounds of dry fuel / 2000 lbs)

9000 =estimated BTU content per pound of dry fuel,

6.24 =estimated mmbtu input per hour (lbs of dry fuel per hour x btu content)

K2

10 =K2 fuel calibration in pounds per count

540 =K2 counts during testing hours

5400 =K2 lbs of wet fuel burned during testing

4.17 =hours during testing

39.7% =average moisture content of fuel

3256 =total pounds of dry fuel burned during testing (wet pounds x (1- moisture content))

781 =lbs of dry fuel burned per hour during testing (pounds of dry fuel / testing hours)

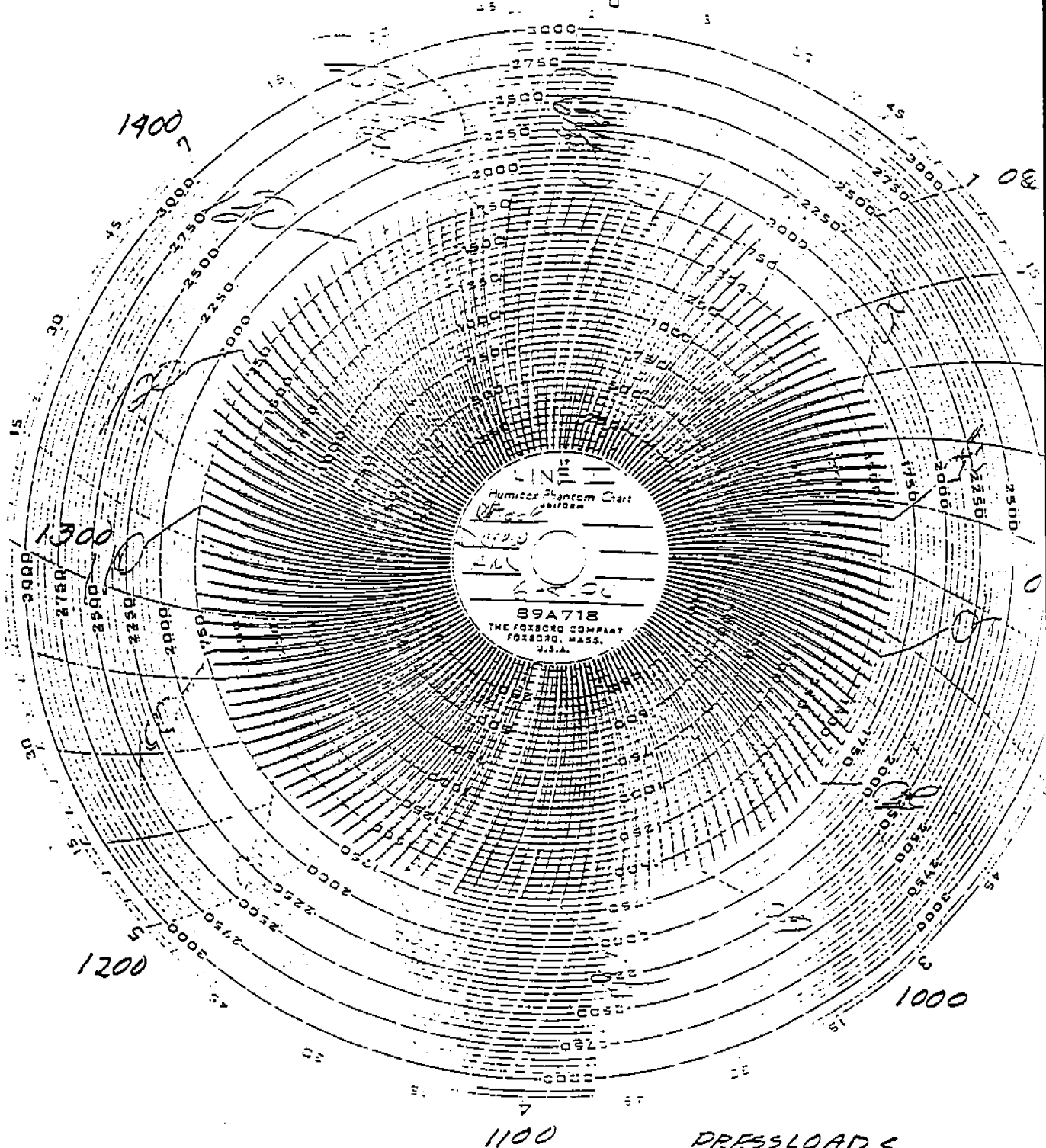
0.39 =tons of dry fuel burned per hour during testing (pounds of dry fuel / 2000 lbs)

9000 =estimated BTU content per pound of dry fuel,

7.03 =estimated mmbtu input per hour (lbs of dry fuel per hour x btu content)

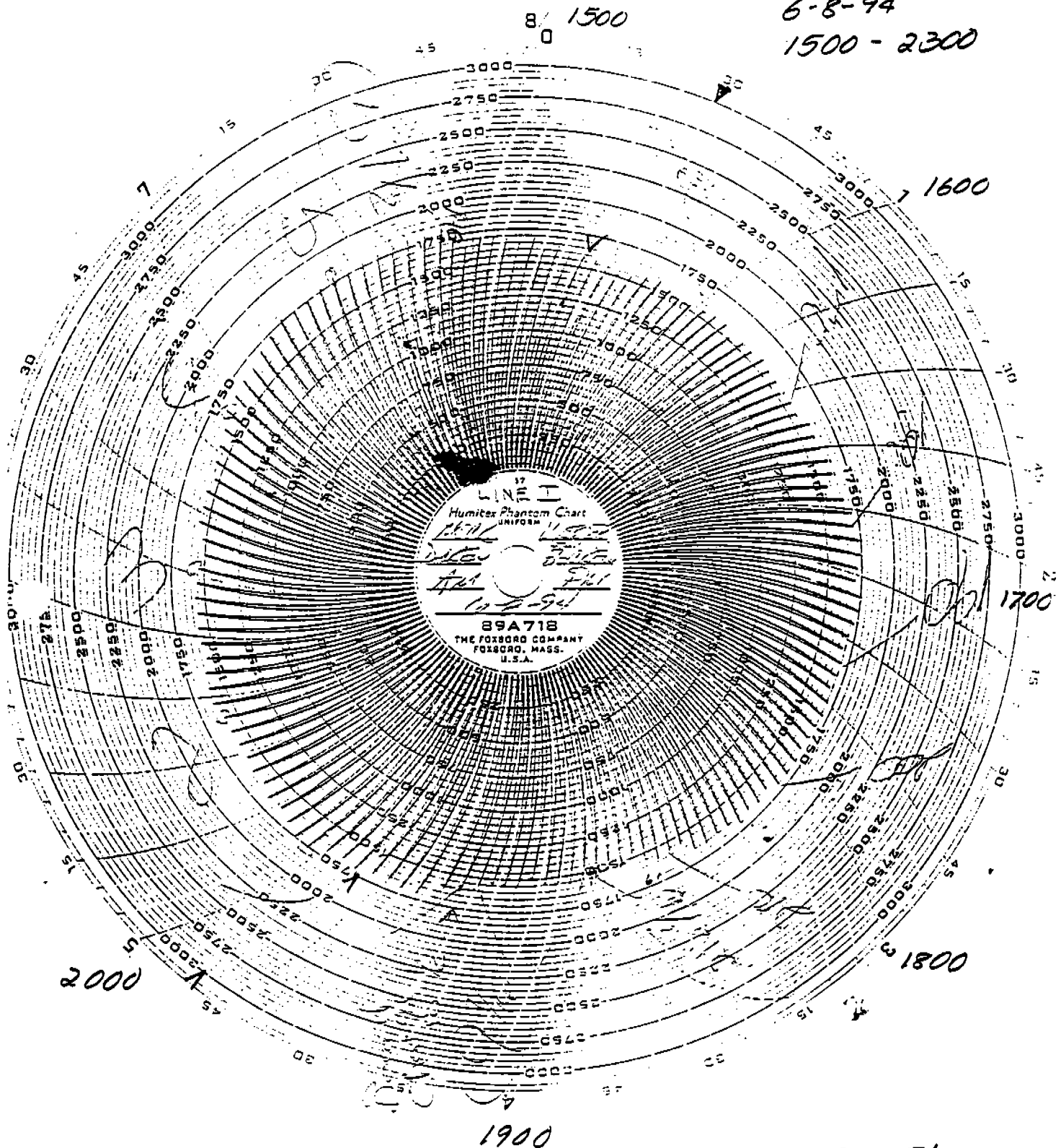
LINE I
PRESS CHAR
6-8-94
0700 - 1500

1500 8 0700



PRESSLOADS
0800 - 1230 = 83

LINE I
 DRESS CHART
 6-8-94
 1500 - 2300



$$1530 - 1950 = 86$$

PREPENS REPORT - Line 1

LINE	SPED	FROM	TO
47		7:00	
50		7:20	
66		8:20	
67		9:30	
66		1:00	

LOG CONTINUED 8830
 F.C.O.S. AND RADIATOR YES
 Cleared Header Struts & Rods YES
 Cleared Deckle Cores YES
 Press Blown Down YES
 Headers Cleared YES
 How Many _____
 Former Byd Radiator YES

[illegible]

Designation Code: M - Mechanical E - Electrical O - Other

PRESS REPORT - LINE 1.

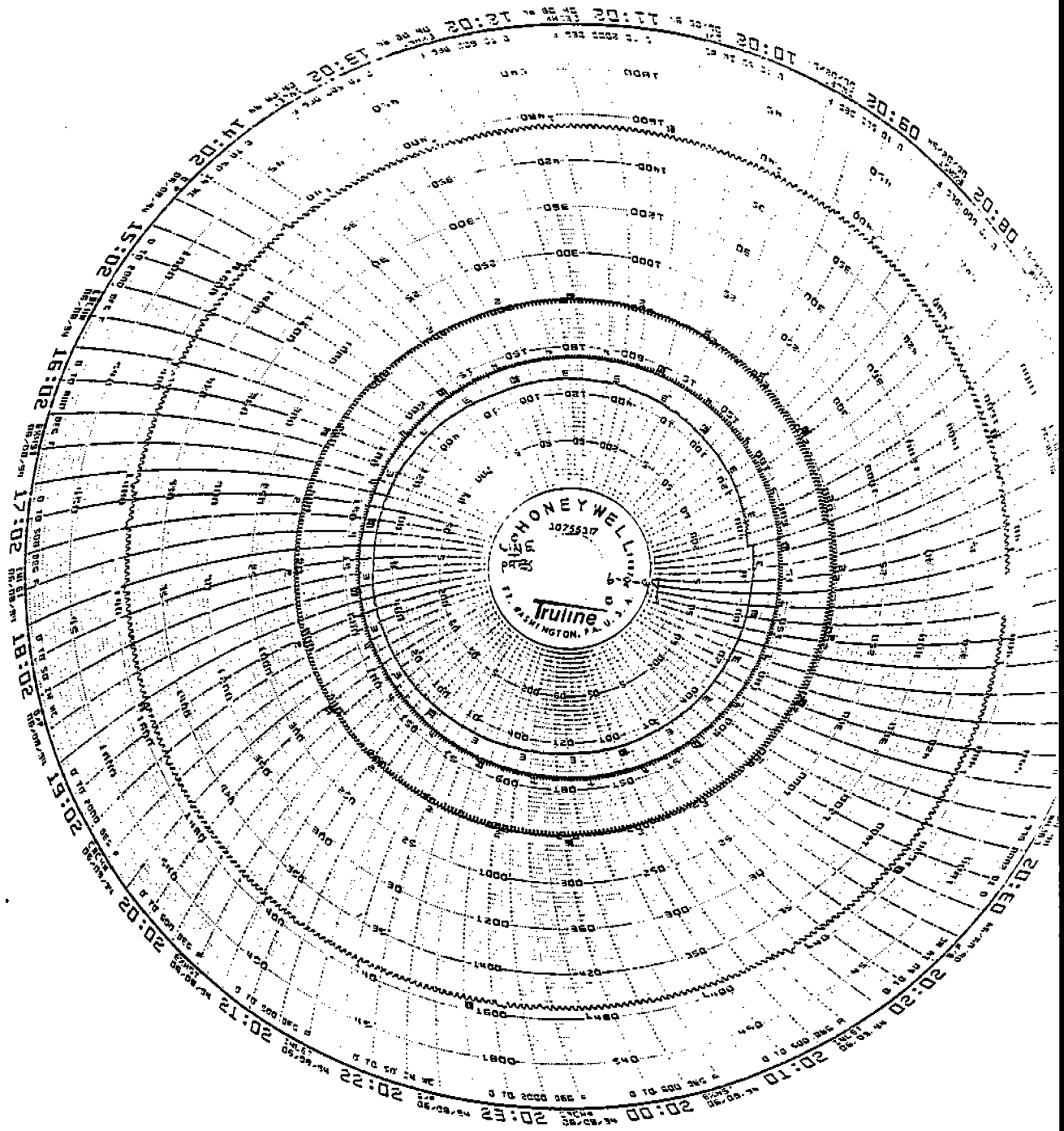
LINE SPEED	FROM	TO
66	7:00	
56 1/2	7:25	
57	1000	
60 3/8	6:25	

LOG CODE: 7469
P.C.S. HD RADIATOR 1130
Cleared Header Switches & Switches YES
Cleared Ductile Cores YES
Pipes Blown Down YES
Headings Cleared YES/NO
How Many
Former Byd Radiator

[illegible]

Downline Code: M - Mechanical E - Electrical O - Other

LINE I
PRESS RTO
CHART
6-8-94



0-2-54 1.1

182

RECOVERY CHAMBER

#1	#2	#3	#4	#5	INLET PRESS.	BURNERS B #1 B #2	INLET TEMP.	COMBUST. CHAMBER TEMP.	EXHAUST TEMP.	ΔP AMP.	GAS
389	421	475	441	432	4.0 W.C.	1589	106	1552	235	14.3	017540
390	421	476	438	416	3.6 W.C.	1585	107	1538	235	13.9	017542
391	423	477	442	433	3.7 W.C.	1615	107	1552	234	14.1	017544
392	422	479	439	417	3.6 W.C.	1570	109	1541	235	13.9	017546
393	421	478	444	432	3.7 W.C.	1612	109	1553	234	14.3	017548
394	423	471	443	416	3.6 W.C.	1588	107	1540	237	13.8	017550
395	421	478	446	458	3.8 W.C.	1620	109	1552	238	14.3	017552
396	421	478	443	471	3.7 W.C.	1591	109	1541	234	13.9	017554
397	424	478	448	461	3.7 W.C.	1619	109	1554	239	14.3	017556
398	424	479	446	418	3.6 W.C.	1576	110	1532	234	13.9	017558
399	424	478	450	466	3.8 W.C.	1620	111	1552	239	14.2	017560
400	424	480	448	459	3.7 W.C.	1580	110	1534	234	13.9	017562
401	424	480	452	477	3.6 W.C.	1612	110	1552	239	13.9	017565
402	425	478	452	448	3.8 W.C.	1570	112	1539	234	13.9	017567
403	424	478	453	470	3.8 W.C.	1607	112	1548	239	13.8	017569
404	426	478	454	431	3.8 W.C.	1576	114	1547	235	14.0	017571
405	425	480	453	419	3.8 W.C.	1576	114	1544	240	13.7	017573
406	427	478	457	439	3.7 W.C.	1612	112	1552	238	14.2	017575
407	425	478	453	498	3.7 W.C.	1602	112	1542	241	13.7	017577
408	426	480	459	441	3.7 W.C.	1622	114	1557	242	14.0	017579
409	427	480	459	441	3.8 W.C.	1596	115	1545	235	13.8	017581
410	426	482	456	501	3.7 W.C.	1591	114	1540	241	13.7	017583
411	428	480	460	443	3.9 W.C.	1617	114	1554	241	14.1	017585
412	426	482	455	491	3.6 W.C.	1578	114	1536	241	13.7	017587
413	428	480	461	460	3.7 W.C.	1623	114	1556	242	14.1	017589
414	427	471	457	468	3.7 W.C.	1578	114	1534	238	13.7	017591

DATA TIME:	START=	08:40	END=	11:30	HOURS=	2.83
	START=	12:40	END=	14:30	HOURS=	1.83
	START=	16:10	END=	18:20	HOURS=	2.17
				total		6.83

weights of approximately every 25th untrimmed board (from press tapes)
19/32 and 15/32" thickness

254	258	199	216	208	227.08 lb=average untrimmed mat weight
246	255	201	218	210	
254	255	209	213	210	
246	258	210	212	214	213 lb=average finished board weight (untrimmed mat weight-weight of trim)
244	259	211	213	211	
242	264	211	212	217	
245	259	209	210	212	
250	263	209	209	208	
250	252	205	212	210	
252	254	209	207		
257	199	214	210		

PLANT PRODUCTION RATE

FUEL BURNING RATE ESTIMATED BY BARK INPUT

10 =K1 fuel calibration in pounds per count
681 =K1 counts during testing hours
6810 =K1 lbs of wet fuel burned during testing
6.83 =hours during testing
37.8% =average moisture content of fuel
4237 =total pounds of dry fuel burned during testing (wet pounds x (1- moisture content))
620 =lbs of dry fuel burned per hour during testing (pounds of dry fuel / testing hours)
0.31 =tons of dry fuel burned per hour during testing (pounds of dry fuel / 2000 lbs)
9000 =estimated BTU content per pound of dry fuel,
5.58 =estimated mmbtu input per hour (lbs of dry fuel per hour x btu content)

10 =K1 fuel calibration in pounds per count
677 =K1 counts during testing hours
6770 =K1 lbs of wet fuel burned during testing
6.83 =hours during testing
37.8% =average moisture content of fuel
4212 =total pounds of dry fuel burned during testing (wet pounds x (1- moisture content))
616 =lbs of dry fuel burned per hour during testing (pounds of dry fuel / testing hours)
0.31 =tons of dry fuel burned per hour during testing (pounds of dry fuel / 2000 lbs)
9000 =estimated BTU content per pound of dry fuel,
5.54 =estimated mmbtu input per hour (lbs of dry fuel per hour x btu content)

LINE 1 THERMAL OIL HEATER - JUNE 9, - PHENOL, BENZENE

DATA TIME: START= 08:40 END= 11:30 HOURS= 2.83
 START= 12:30 END= 13:20 HOURS= 0.83
 total= 3.67

BOARD WEIGHTS - LBS

weights of approximately every 25th untrimmed board (from press tapes)
 7/16 and 1/2"

254	257	252	244.11 lb=average
246	258	254	untrimmed
254	255	199	mat weight
246	255	199	
244	258	201	228.98 lb=average
242	259	209	finished board
245	264	210	weight
250	259		(untrimmed mat
250	263		weight-weight
252	256		of trim)

6.2% =trim %

PLANT PRODUCTION RATE

3.67 =hours during testing
 53 =pressloads
 636 =no. of 8'x16' boards produced (pressloads x 12 boards per load)
 145631 =lbs of finished product (boards produced x weight of finished board)
 39718 =lbs of finished product per hour (lbs of finished product / hours)
 19.86 =tons of finished product per hour (lbs of finished product per hour / 2000 lb)

FUEL BURNING RATE ESTIMATED BY BARK INPUT

K1

10 =K1 fuel calibration in pounds per count
 314 =K1 counts during testing hours
 3140 =K1 lbs of wet fuel burned during testing
 3.67 =hours during testing
 38.0% =average moisture content of fuel
 1946 =total pounds of dry fuel burned during testing (wet pounds x (1- moisture content))
 531 =lbs of dry fuel burned per hour during testing (pounds of dry fuel / testing hours)
 0.27 =tons of dry fuel burned per hour during testing (pounds of dry fuel / 2000 lbs)
 9000 =estimated BTU content per pound of dry fuel,
 4.78 =estimated mmbtu input per hour (lbs of dry fuel per hour x btu content)

K2

10 =K2 fuel calibration in pounds per count
 296 =K2 counts during testing hours
 2960 =K2 lbs of wet fuel burned during testing
 3.67 =hours during testing
 38.0% =average moisture content of fuel
 1834 =total pounds of dry fuel burned during testing (wet pounds x (1- moisture content))
 500 =lbs of dry fuel burned per hour during testing (pounds of dry fuel / testing hours)
 0.25 =tons of dry fuel burned per hour during testing (pounds of dry fuel / 2000 lbs)
 9000 =estimated BTU content per pound of dry fuel,
 4.5 =estimated mmbtu input per hour (lbs of dry fuel per hour x btu content)

LINE 1 THERMAL OIL HEATER - JUNE 9, - FORMALDEHYDE

DATA TIME: START= 13:40 END= 14:20 HOURS= 0.67
 START= 16:30 END= 19:00 HOURS= 2.50
 total 3.17

BOARD WEIGHTS - LBS

weights of approximately every 25th untrimmed board (from press tapes)

211	209	212	211.56 lb=average
209	212	208	untrimmed
209	207	210	mat weight
205	210	215	
209	208	215	198.44 lb=average
214	210	220	finished board
216	210	216	weight
213	214		(untrimmed mat
212	211		weight-weight
210	217		of trim)

6.2% =trim %

PLANT PRODUCTION RATE

3.17 =hours during testing
 56 =pressloads
 672 =no. of 8'x16' boards produced (pressloads x)2boards per load)
 133352 =lbs of finished product (boards produced x weight of finished board)
 42111 =lbs of finished product per hour (lbs of finished product / hours)
 21.06 =tons of finished product per hour (lbs of finished product per hour / 2000 lb)

FUEL BURNING RATE ESTIMATED BY BARK INPUT

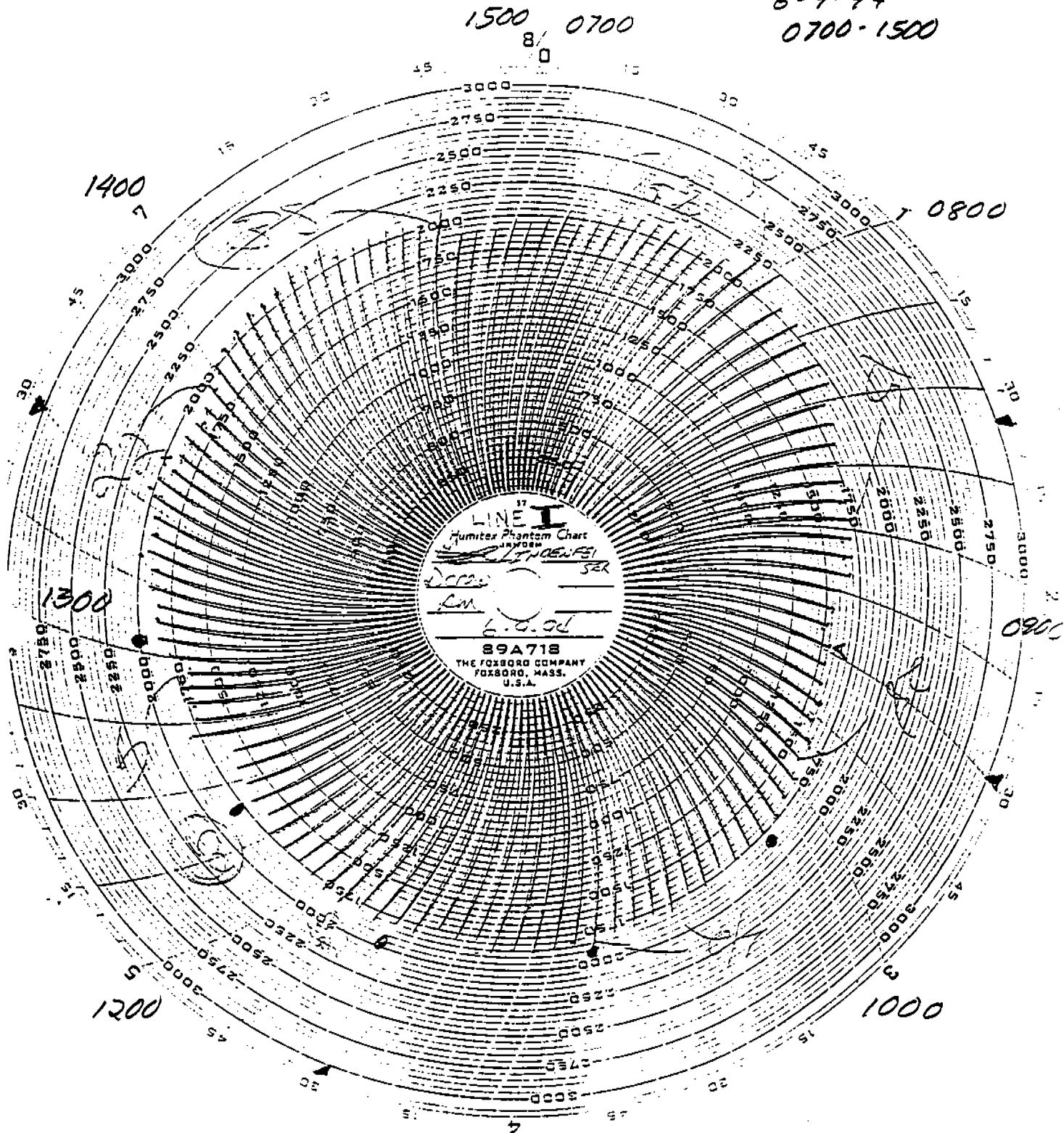
K1

10 =K1 fuel calibration in pounds per count
 286 =K1 counts during testing hours
 2860 =K1 lbs of wet fuel burned during testing
 3.17 =hours during testing
 38.3% =average moisture content of fuel
 1765 =total pounds of dry fuel burned during testing (wet pounds x (1- moisture content))
 557 =lbs of dry fuel burned per hour during testing (pounds of dry fuel / testing hours)
 0.28 =tons of dry fuel burned per hour during testing (pounds of dry fuel / 2000 lbs)
 9000 =estimated BTU content per pound of dry fuel,
 5.01 =estimated mmbtu input per hour (lbs of dry fuel per hour x btu content)

K2

10 =K1 fuel calibration in pounds per count
 302 =K1 counts during testing hours
 3020 =K1 lbs of wet fuel burned during testing
 3.17 =hours during testing
 38.3% =average moisture content of fuel
 1864 =total pounds of dry fuel burned during testing (wet pounds x (1- moisture content))
 589 =lbs of dry fuel burned per hour during testing (pounds of dry fuel / testing hours)
 0.29 =tons of dry fuel burned per hour during testing (pounds of dry fuel / 2000 lbs)
 9000 =estimated BTU content per pound of dry fuel,
 5.3 =estimated mmbtu input per hour (lbs of dry fuel per hour x btu content)

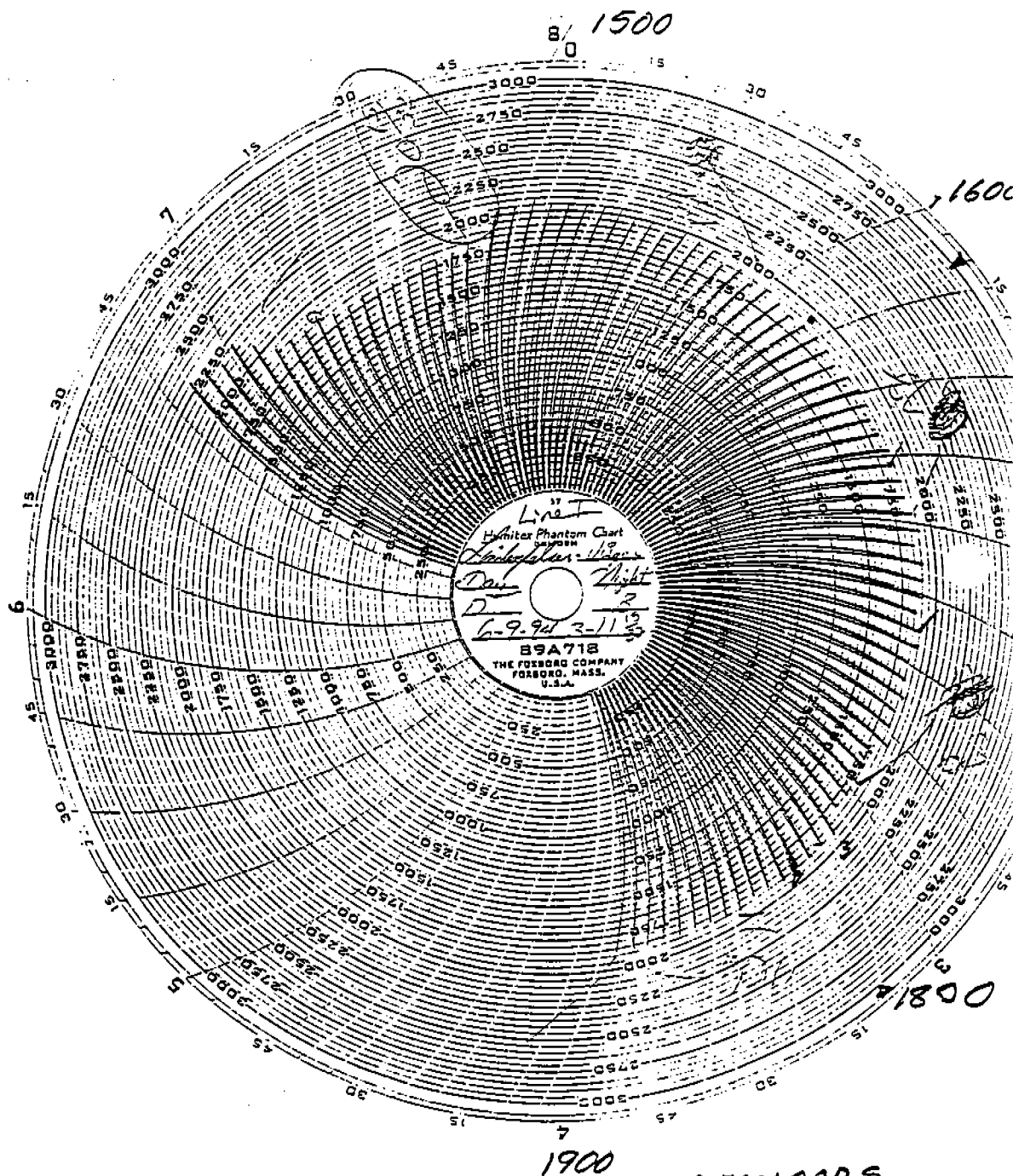
LINE I
DRESS CHART
6-9-94
0700-1500



$$1340-1420 = 12$$

$$\begin{aligned} 0930-1330 &= 57 \\ 0840-1130 &= 40 \\ 1240-1430 &= 31 \\ 1230-1320 &= 13 \end{aligned}$$

LINE I
PRESS CHART
6-9-94
1500-2300



PRESSLOADS
1610 - 1820 = 36
1630 - 1900 = 43

PRESS REPORT - LINE 1

OPERATOR LindenFelsner

Summary

Am

53

2005

6.9-94

3/8

PRESS LOADS 153/8 - 65 19/32 106 1/4

OVERALL TMR: 152

~~DISCONTINUED FILE~~ 15

PRESS MAP: 210

THE INDEX

LOG CODE: 8487

T.C.O.S. END RADIATOR 8:46

Classed Member Summary & Remarks

Closed Deckle Cards

Print Along Down 8-55

~~Heads-up Closed~~-----YES/NO

~~How Many~~

Forward End Radiation

LINE SPEED	FROM	TO
60 $\frac{3}{8}$	7:00	7:49
47 $\frac{1}{32}$	7:49	12:45
58 $\frac{1}{32}$	12:45	7:00

$$\frac{3}{8} = 384,637.$$
[illegible]

Downline Code: X - Mechanical

E - English

0 - ~~CONFIDENTIAL~~

26

LINE 1 PRESS TESTING JUNE 10, 1994 - TSP, VOC, CO, NOX

DATA TIME START= 09:30 END= 13:30 HOURS= 4.00

BOARD WEIGHTS - LBS

weights of approximately every 25th untrimmed board (from press tapes)

19/32&15/32

194	190	200	191	192.18 lb=average
194	187	193	193	untrimmed
197	185	196	193	mat weight
191	189	197	190	
189	185	195	189	180.26 lb=average
189	191	198	194	finished board
187	192	199	188	weight
190	201	189		(untrimmed mat
189	197	192		weight-weight
188	192	192		of trim)

6.2% =trim %

PLANT PRODUCTION RATE

4.00 =hours during testing

70 =pressloads

840 =no. of 8'x16' boards produced (pressloads x12 boards per load)

151418 =lbs of finished product (boards produced x weight of finished board)

37855 =lbs of finished product per hour (lbs of finished product / hours)

18.93 =tons of finished product per hour (lbs of finished product per hour / 2000 lb)

$$\frac{840 \times 8 \times 16}{4} = 2688 \frac{\text{msf}}{\text{hr}} \times \frac{7}{16}$$

RESIN USAGE FROM TANK MEASUREMENTS

Note: common tanks supply wax and resin to both Line 1 and Line 2. Usage for one line is estimated by proportioning the total usage by the footage (3/8" basis) for each line)

MEASUREMENT SUMMARY:

				PHENOLIC	PHENOLIC	WAX	WAX
				61%	100%	58%	100%
				solids	solids	solids	solids
	line 1	line 2	MDI	lbs	lbs	lbs	lbs
time	footage	footage	lbs				
09:00	32257	30465	820	2376	1449	1527	886
10:00	28673	32257	521	2497	1523	764	443
11:00	32257	30465	522	2508	1530	764	443
12:00	34049	30465	745	2285	1394	1145	664
13:00	30465	8960	149	1436	876	382	222
14:00	28673	28673	669	2335	1424	1146	665
hourly							
average	31062	26881	571	2240	1366	955	554
Line 1			341		816		331
Line 2			230		550		223

37855 =average lbs. per hour finished product produced during testing

341 =average lbs. per hour of MDI resin used during testing

0.90% = MDI resin used as % of finished product

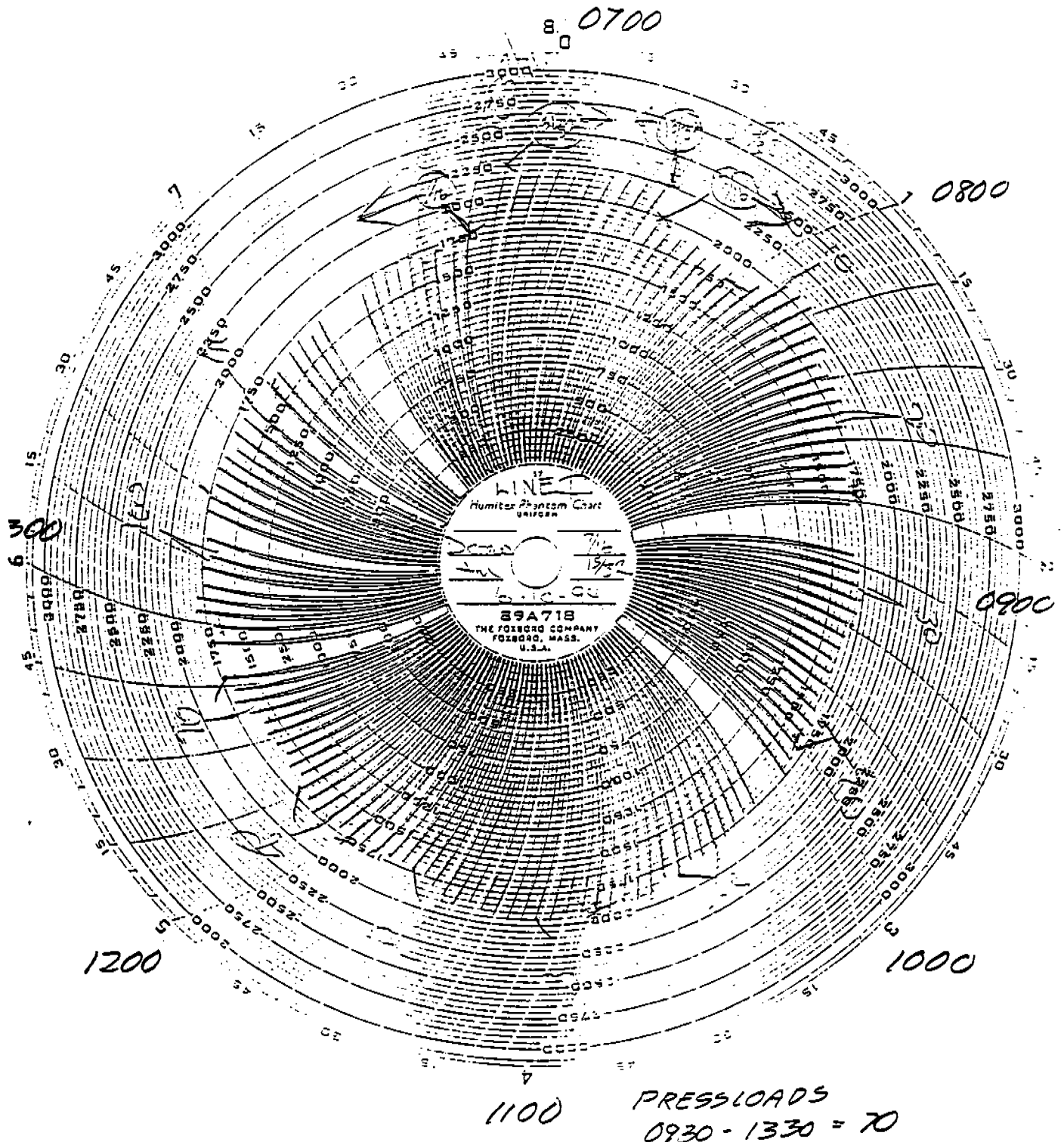
816 =average lbs. per hour of phenolic resin (100% solids) used during testing

2.16% =Phenolic resin used as % of finished product

331 =average lbs. per hour of wax (100% solids) used during testing

0.87% =wax used as % of finished product

LINE I
PRESS CHART
6-10-94
0700 - 1500



LOUISIANA-PACIFIC CORPORATION
HAYWARD, MI

PRESS REPORT - LI

OPERATOR MAN SUTER SHIFT DAYS GEN 10 DATE 6-11
THICKNESS: 15/37 7/16 PRESS LOADS 1015/37 1407/16 18
OVERALL TIME: 165-138 DECOMPRESSION TIME 17
PRESS TEMP: 210 TOTAL REELS: =
LOG COUNT: 6717

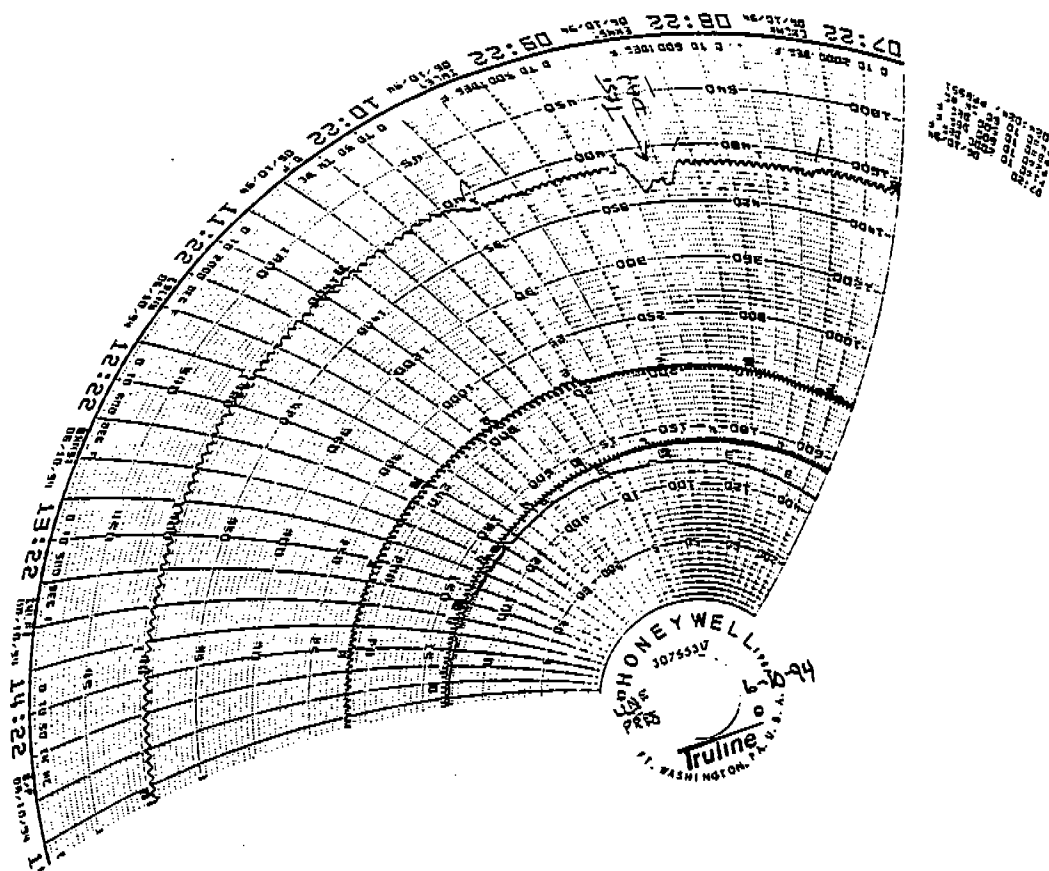
LINE SPEED	FROM	TO
58	7:00	
65	7:32	7/16
36	3:48	23/32 SE
25	5:15	

P.C.O.S. BY RADIATOR 8:10
Cleaned Header Struts & Tracks =
Cleaned Deckle Cases =
Press Blow Down 8:10
Headbars Cleaned = YES/NO =
How Many =
Former Eyd Radiator =

DOWNTIME		DOWNTIME (Mins)			X Z Y	REASONS FOR DOWNTIME
FROM	TO	M	E	O		
8:04	8:15				11	BLAKE AT SAWS
10:15	10:18				3	LINET NOT MADE F#1, 6
12:50	12:56				6	LOWER LINET F#7 (ASSN)
1:22	1:23				1	LID. OVERTRAVEL
1:33	1:34				2	NO AUTO INDEX
1:48	1:49				1	" " "
1:54	1:56				2	" " "
2:04	2:06				2	ADJUST LINETS
2:18	2:20				8	ADJUSTING LID.
2:28	2:29				1	F#7 NOT MADE...
2:57	2:57				1	DROPPED H B F#12 LOAD
5:29	6:46				76	RTO DEVERS DOWN

Downtime Code: M - Mechanical E - Electrical O - Operator

LINE I
PRESS RTO
CHART
6-10-94



LINE I PRESS 6-10-94

#1	#2	#3	#4	#5	INLET PRESS.	BURNERS B #1	BURNERS B #2	INLET TEMP.	COMBUST. CHAMBER TEMP.	EXHAUST TEMP.	AMP.	GAS.
399	420	478	453	458	3.7	1583	1592	113	1537	235	14.1	017933
8:15	420	477	457	488	3.7	1582	1574	114	1532	240	13.7	017935
8:30	423	478	461	445	3.8	1578	1566	115	1536	237	13.9	017937
8:45	424	482	460	489	3.7	1553	1576	116	1523	243	13.8	017940
9:00	425	482	467	444	3.8	1596	1566	116	1546	243	13.9	017942
9:15	427	483	468	462	3.8	1485	1501	117	1469	241	13.7	017943
9:30	428	481	475	461	3.8	1622	1596	116	1548	246	13.9	017946
9:45	430	481	477	445	3.8	1558	1541	117	1519	242	13.6	017947
10:00	430	482	477	493	3.7	1554	1554	119	1516	245	13.6	017949
10:15	432	483	475	506	3.6	1540	1555	122	1506	248	13.6	017951
10:30	434	482	478	481	3.5	1530	1546	119	1514	247	13.8	017954
10:45	439	482	485	456	3.7	1620	1589	121	1569	252	13.4	017957
11:00	444	482	484	485	3.6	1606	1592	120	1541	253	13.4	017959
11:15	441	484	474	4531	3.5	1568	1577	121	1554	253	13.4	017962
11:30	442	483	481	466	3.7	1581	1587	123	1558	248	13.7	017964
11:45	442	482	498	448	3.8	1618	1586	122	1568	254	13.3	017966
12:00	441	485	488	486	3.4	1604	1599	123	1564	255	13.3	017969
12:15	441	489	481	533	3.4	1567	1596	122	1554	257	13.3	017971
12:30	444	486	494	458	3.5	1615	1593	123	1568	257	13.2	017973
12:45	443	489	492	502	3.6	1598	1596	123	1561	257	13.3	017976
1:00	445	491	489	496	3.4	1566	1586	124	1552	257	13.5	017978
1:15	444	494	487	529	3.5	1562	1590	124	1552	258	13.2	017980
1:30	445	494	491	541	3.4	1570	1593	123	1554	258	13.2	017982
1:45												
2:00												
2:15												

LINE 2 THERMAL OIL HEATER JUNE 7, - POM

DATA TIME: START= 08:20 END= 13:40 HOURS= 5.33
 START= 14:25 END= 16:30 HOURS= 2.08
 total 7.42

BOARD WEIGHTS - LBS

weights of approximately every 25th untrimmed board (from press tapes)
 7/16"

198	198	198	196	194 lb=average
200	192	196	192	untrimmed
196	194	196	196	mat weight
194	190	188	200	
194	200	192	202	178.67 lb=average
192	200	192	196	finished board
192	198	190	188	weight
194	202	188	194	(untrimmed mat
190	204	186	194	weight-weight
192	204	188	184	of trim)
194	208	190	196	
190	192	190	182	7.9% =trim %
192	196	192	190	
192	198	190		
190	196	194		

PLANT PRODUCTION RATE

7.42 =hours during testing
 122 =pressloads
 1464 =no. of 8'x16' boards produced (pressloads x 12boards per load)
 261573 =lbs of finished product (boards produced x weight of finished board)
 35269 =lbs of finished product per hour (lbs of finished product / hours)
 17.63 =tons of finished product per hour (lbs of finished product per hour / 2000 lb)
 note -press down from

FUEL BURNING RATE ESTIMATED BY BARK INPUT

K3

10 =K3 fuel calibration in pounds per count
 1460 =K3 counts during testing hours
 14600 =K3 lbs of wet fuel burned during testing
 5.33 =hours during testing
 39.4% =average moisture content of fuel
 8843 =total pounds of dry fuel burned during testing (wet pounds x (1- moisture content))
 1658 =lbs of dry fuel burned per hour during testing (pounds of dry fuel / testing hours)
 0.83 =tons of dry fuel burned per hour during testing (pounds of dry fuel / 2000 lbs)
 9000 =estimated BTU content per pound of dry fuel,
 14.92 =estimated mmbtu input per hour (lbs of dry fuel per hour x btu content)

K4

10 =K4 fuel calibration in pounds per count
 358 =K4 counts during testing hours
 3580 =K4 lbs of wet fuel burned during testing
 5.33 =hours during testing
 39.4% =average moisture content of fuel
 2168 =total pounds of dry fuel burned during testing (wet pounds x (1- moisture content))
 407 =lbs of dry fuel burned per hour during testing (pounds of dry fuel / testing hours)
 0.2 =tons of dry fuel burned per hour during testing (pounds of dry fuel / 2000 lbs)
 9000 =estimated BTU content per pound of dry fuel,
 3.66 =estimated mmbtu input per hour (lbs of dry fuel per hour x btu content)

LINE 2 THERMAL OIL HEATER JUNE 7, BENZENE

DATA TIME: START= 08:50 END= 12:40 HOURS= 3.83
 START= 14:30 END= 15:40 HOURS= 1.17
 total 5.00

BOARD WEIGHTS - LBS

weights of approximately every 25th untrimmed board (from press tapes)

7/16"

192	200	192	196
192	198	190	188
194	202	188	
190	204	186	
192	204	188	
194	208	190	
190	192	190	
192	196	192	
192	198	190	
190	196	194	
198	198	196	
192	196	192	
194	196	196	
190	188	200	
200	192	202	

194.26 lb=average
untrimmed
mat weight

178.91 lb=average
finished board
weight
(untrimmed mat
weight-weight
of trim)

7.9% =trim %

PLANT PRODUCTION RATE

5.00 =hours during testing

95 =pressloads

1140 =no. of 8'x16' boards produced (pressloads x12 boards per load)

203957 =lbs of finished product (boards produced x weight of finished board)

40792 =lbs of finished product per hour (lbs of finished product / hours)

20.40 =tons of finished product per hour (lbs of finished product per hour / 2000 lb)

note -press down from

FUEL BURNING RATE ESTIMATED BY BARK INPUT

K3

10 =K3 fuel calibration in pounds per count

974 =K3 counts during testing hours

9740 =K3 lbs of wet fuel burned during testing

3.83 =hours during testing

38.9% =average moisture content of fuel

5949 =total pounds of dry fuel burned during testing (wet pounds x (1- moisture content))

1552 =lbs of dry fuel burned per hour during testing (pounds of dry fuel / testing hours)

0.78 =tons of dry fuel burned per hour during testing (pounds of dry fuel / 2000 lbs)

9000 =estimated BTU content per pound of dry fuel,

13.97 =estimated mmbtu input per hour (lbs of dry fuel per hour x btu content)

K4

10 =K4 fuel calibration in pounds per count

247 =K4 counts during testing hours

2470 =K4 lbs of wet fuel burned during testing

3.83 =hours during testing

38.9% =average moisture content of fuel

1509 =total pounds of dry fuel burned during testing (wet pounds x (1- moisture content))

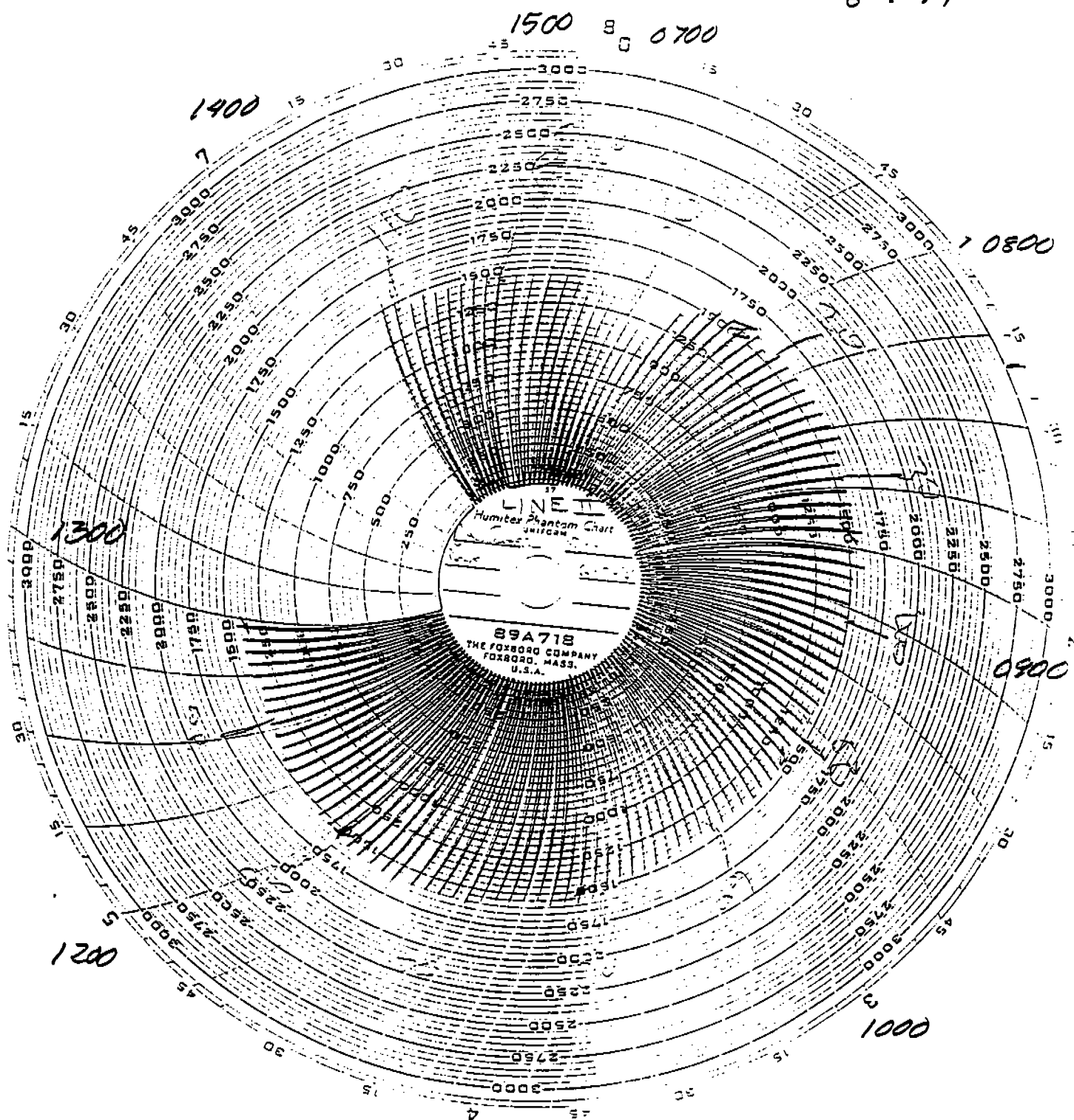
394 =lbs of dry fuel burned per hour during testing (pounds of dry fuel / testing hours)

0.2 =tons of dry fuel burned per hour during testing (pounds of dry fuel / 2000 lbs)

9000 =estimated BTU content per pound of dry fuel,

3.55 =estimated mmbtu input per hour (lbs of dry fuel per hour x btu content)

LINE II
PRESS CHART
6-7-94



1430-1500 = 9

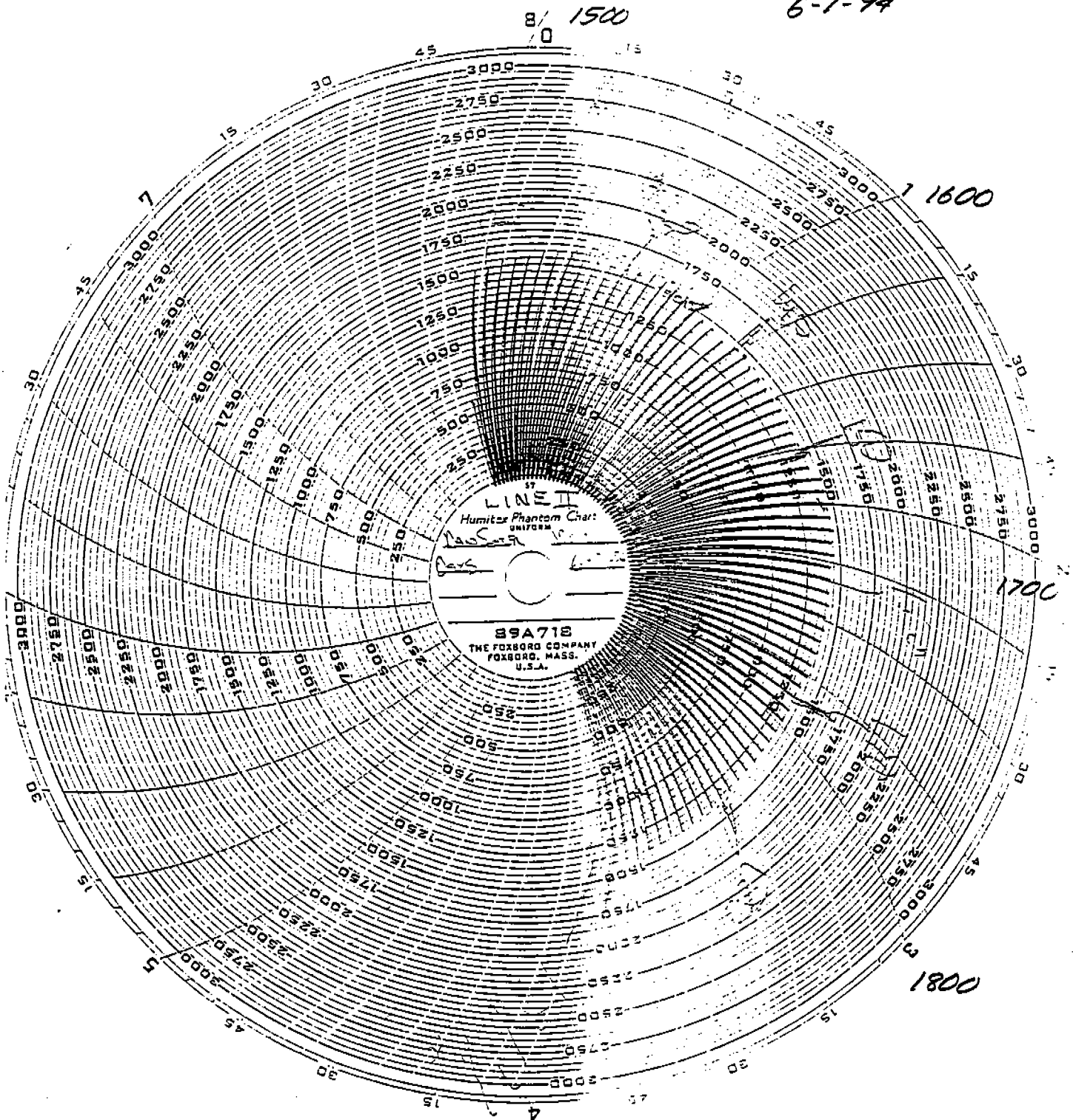
PRESSLOADS

0820-1320 = 85

1425-1500 = 10

0850-1240 = 74

LINE II
PRESS CHART
6-7-94



$$1500 - 1630 = 27$$

$$1500 - 1540 = 12$$

PRESS REPORT - LINE 17

LINE SPEED	FROM	TO
51	7:00	
60	7:15	
40	17:59	
69		

[illegible]

36

LINE 2 THERMAL OIL HEATER - JUNE 8, - PHENOL, FORMALDEHYDE
 DATA TIME: START= 14:40 END= 18:50 HOURS= 4.17

BOARD WEIGHTS - LBS

weights of approximately every 25th untrimmed board (from press tapes)
 7/16"

196	192	192	190
202	208	194	190
206	198	198	188
206	192	196	
194	192	196	
198	196	198	
202	192	198	
200	194	188	
200	198	190	
200	194	190	

196 lb=average
 untrimmed
 mat weight

180.52 lb=average
 finished board
 weight
 (untrimmed mat
 weight-weight
 of trim)

7.9% =trim %

PLANT PRODUCTION RATE

4.17 =hours during testing
 66 =pressloads
 792 =no. of 8'x16' boards produced (pressloads x12 boards per load)
 142972 =lbs of finished product (boards produced x weight of finished board)
 34314 =lbs of finished product per hour (lbs of finished product / hours)
 17.16 =tons of finished product per hour (lbs of finished product per hour / 2000 lb)
 note -press down from

FUEL BURNING RATE ESTIMATED BY BARK INPUT

K3

10 =K3 fuel calibration in pounds per count
 604 =K3 counts during testing hours
 6040 =K3 lbs of wet fuel burned during testing
 4.17 =hours during testing
 38.5% =average moisture content of fuel
 3713 =total pounds of dry fuel burned during testing (wet pounds x (1- moisture content))
 891 =lbs of dry fuel burned per hour during testing (pounds of dry fuel / testing hours)
 0.45 =tons of dry fuel burned per hour during testing (pounds of dry fuel / 2000 lbs)
 9000 =estimated BTU content per pound of dry fuel,
 8.02 =estimated mmbtu input per hour (lbs of dry fuel per hour x btu content)

K4

10 =K4 fuel calibration in pounds per count
 79 =K4 counts during testing hours
 790 =K4 lbs of wet fuel burned during testing
 4.17 =hours during testing
 38.5% =average moisture content of fuel
 486 =total pounds of dry fuel burned during testing (wet pounds x (1- moisture content))
 117 =lbs of dry fuel burned per hour during testing (pounds of dry fuel / testing hours)
 0.06 =tons of dry fuel burned per hour during testing (pounds of dry fuel / 2000 lbs)
 9000 =estimated BTU content per pound of dry fuel,
 1.05 =estimated mmbtu input per hour (lbs of dry fuel per hour x btu content)

page missing in orig. report

LINE 2 THERMAL OIL HEATER JUNE 8, - TSP, CO, NOX

DATA TIME: START= 08:00 END= 12:20 HOURS= 4.33

YARD WEIGHTS - LBS

Weights of approximately every 25th untrimmed board (from press tapes)

7/16"

198	190	194	184	190.89 lb=average
194	188	196	190	untrimmed
196	186	192	188	mat weight
200	188	190	188	
204	188	188	190	175.81 lb=average
204	188	188	198	finished board
200	190	182	190	weight
192	192	182	186	(untrimmed mat
188	190	186		weight-weight
188	188	190		of trim)

7.9% =trim %

PLANT PRODUCTION RATE

4.33 =hours during testing

79 =pressloads

948 =no. of 8'x16' boards produced (pressloads x 8 boards per load)

166668 =lbs of finished product (boards produced x weight of finished board)

38462 =lbs of finished product per hour (lbs of finished product / hours)

19.23 =tons of finished product per hour (lbs of finished product per hour / 2000 lb)

note -press down from

EL BURNING RATE ESTIMATED BY BARK INPUT

K3

10 =K3 fuel calibration in pounds per count

801 =K3 counts during testing hours

8010 =K3 lbs of wet fuel burned during testing

4.33 =hours during testing

39.8% =average moisture content of fuel

4819 =total pounds of dry fuel burned during testing (wet pounds x (1- moisture content))

1112 =lbs of dry fuel burned per hour during testing (pounds of dry fuel / testing hours)

0.56 =tons of dry fuel burned per hour during testing (pounds of dry fuel / 2000 lbs)

9000 =estimated BTU content per pound of dry fuel,

10.01 =estimated mmbtu input per hour (lbs of dry fuel per hour x btu content)

K4

10 =K4 fuel calibration in pounds per count

197 =K4 counts during testing hours

1970 =K4 lbs of wet fuel burned during testing

4.33 =hours during testing

39.8% =average moisture content of fuel

1185 =total pounds of dry fuel burned during testing (wet pounds x (1- moisture content))

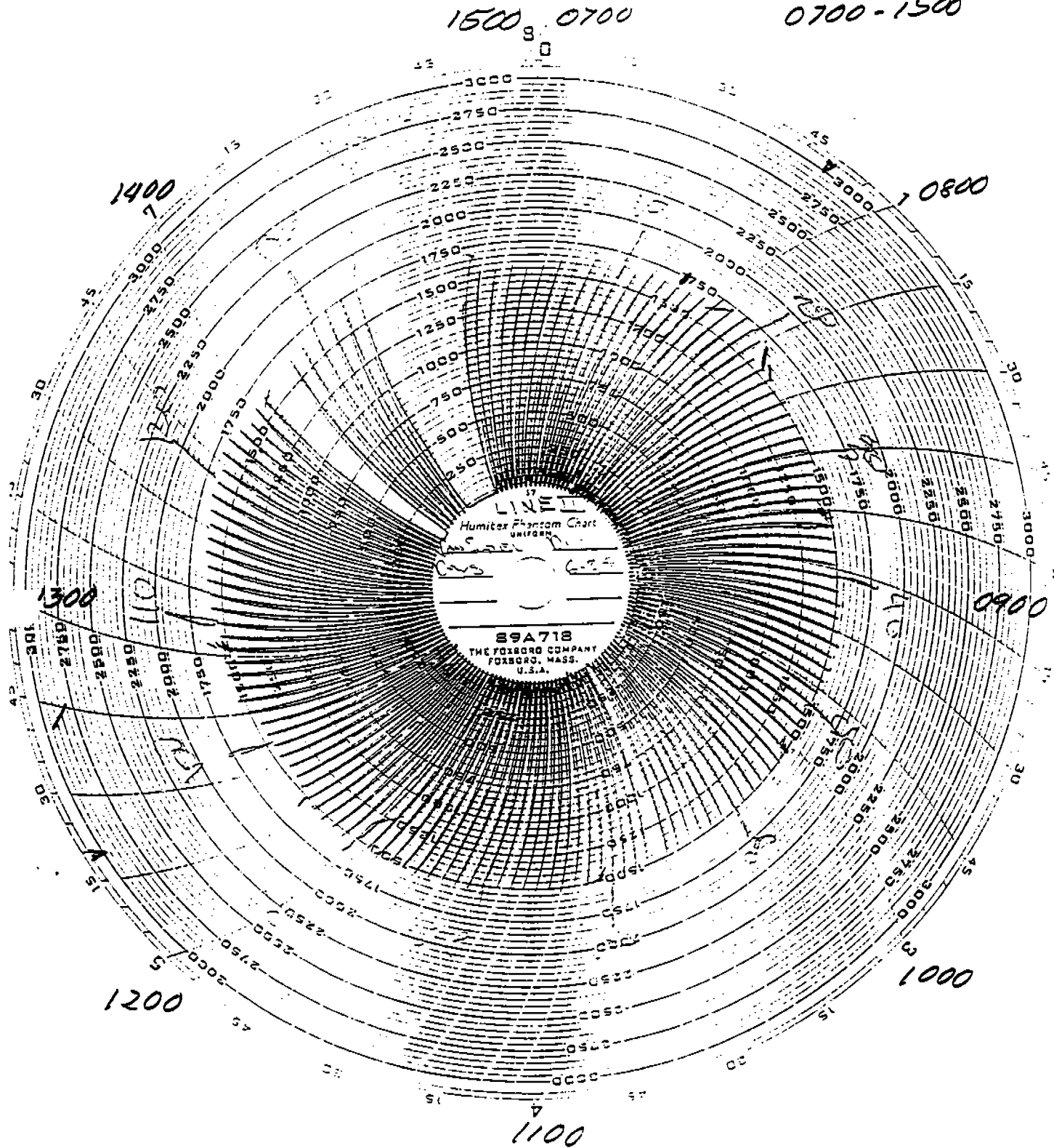
273 =lbs of dry fuel burned per hour during testing (pounds of dry fuel / testing hours)

0.14 =tons of dry fuel burned per hour during testing (pounds of dry fuel / 2000 lbs)

9000 =estimated BTU content per pound of dry fuel,

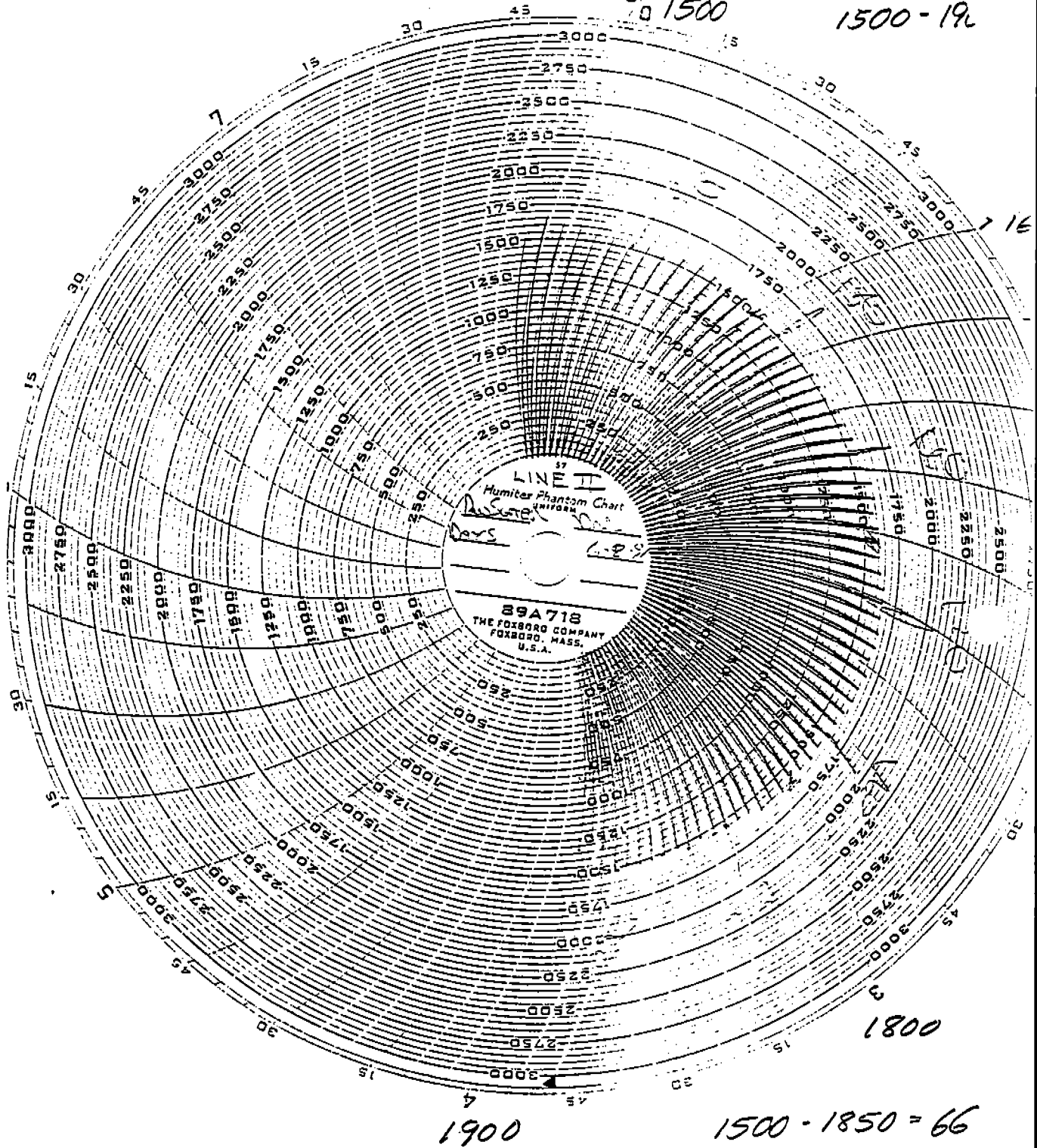
2.46 =estimated mmbtu input per hour (lbs of dry fuel per hour x btu content)

LINE II
PRESS CHART
6-8-94
0700-1500



0800-1220 = 79
1440-1500 = 0

LINE II
PRESS CHART
6-8-94
1500-19



PRESS REPORT - LINE 1

LINE SPEED	FROM	TO
55	2:00	
64	2:30	
50	2:10	
64	3:58	

PRESS LOOPS 10/11/16
 DECOMPRESSION TIME 10
 TOTAL REPAIRS: 3
 LOG CODE: 7099
 P.C.O.S. BYD RADIATOR 9:30
 Cleared Hander Struts & Brakes =
 Cleared Double Chairs =
 Press Blown Down 9:30
 Headband Cleared = YES/NO
 Hot Mary =
 Former Byd Radiator =

[illegible]

Downline Code: M - Mechanical E - Electrical O - Operator

DATA TIME: START= 12:40 END= 17:20 HOURS= 4.67

BOARD WEIGHTS - LBS

weights of approximately every 25th untrimmed board (from press tapes)
7/16"

196	197	184	190
193	194	186	195
196	193	188	193
196	191	188	194
195	191	184	193
195	185	191	196
193	186	186	192
194	189	187	195
195	189	190	196
193	186	189	194

191.45 lb=average
untrimmed
mat weight

176.33 lb=average
finished board
weight
(untrimmed mat
weight-weight
of trim)

7.9% =trim %

PLANT PRODUCTION RATE

4.67 =hours during testing
84 =pressloads
1008 =no. of 8'x16' boards produced (pressloads x 12 boards per load)
177741 =lbs of finished product (boards produced x weight of finished board)
38088 =lbs of finished product per hour (lbs of finished product / hours)
19.04 =tons of finished product per hour (lbs of finished product per hour / 2000 lb)

RESIN USAGE FROM TANK MEASUREMENTS

Note: common tanks supply wax and resin to both Line 1 and Line 2. Usage for one line is estimated by proportioning the total usage by the footage (3/8" basis) for each line)

MEASUREMENT SUMMARY:

				PHENOLIC	PHENOLIC	WAX	WAX
				61%	100%	58%	100%
	line 1	line 2	MDI	solids	solids	solids	solids
time	footage	footage	lbs	lbs	lbs	lbs	lbs
12:00	31615	28673	521	2527	1541	1336	815
13:00	33919	21505	596	2123	1295	764	466
14:00	32640	34049	671	2898	1768	955	583
15:00	30720	32257	669	2234	1363	954	582
16:00	32640	32257	671	2426	1480	1337	816
17:00	32640	32257	745	3272	1996	763	465
18:00	32640	34049	670	1719	1049	1146	699
hourly							
average	32402	30721	649	2457	1499	1036	632
Line 1			333		769		325
Line 2			316		729		308

38088 =average lbs. per hour finished product produced during testing
316 =average lbs. per hour of MDI resin used during testing
0.83% = MDI resin used as % of finished product

729 =average lbs. per hour of phenolic resin (100% solids) used during testing
1.92% =Phenolic resin used as % of finished product

308 =average lbs. per hour of wax (100% solids) used during testing
0.81% =wax used as % of finished product

LINE 2 PRESS TESTING JUNE 9, 1994 - MDI

DATA TIME: START= 13:20 END= 18:30 HOURS= 5.17

BOARD WEIGHTS - LBSweights of approximately every 25th untrimmed board (from press tapes)
7/16"

192	190	200
190	190	194
190	188	188
190	190	194
194	188	194
184	190	196
192	186	188
190	184	190
190	194	196
194	192	

190.97 lb=average
untrimmed
mat weight175.88 lb=average
finished board
weight
(untrimmed mat
weight-weight
of trim)

7.9% =trim %

PLANT PRODUCTION RATE

5.17 =hours during testing

93 =pressloads

1116 =no. of 8'x16' boards produced (pressloads x 12boards per load)

196282 =lbs of finished product (boards produced x weight of finished board)

37990 =lbs of finished product per hour (lbs of finished product / hours)

19.00 =tons of finished product per hour (lbs of finished product per hour / 2000 lb)

*27.63 M.F. / hr 7/16*RESIN USAGE FROM TANK MEASUREMENTS

Note: common tanks supply wax and resin to both Line 1 and Line 2. Usage for one line is estimated by proportioning the total usage by the footage (3/8" basis) for each line)

MEASUREMENT SUMMARY:

	line 1	line 2	MDI	PHENOLIC 61%	PHENOLIC 100%	WAX 58%	WAX 100%
	footage	footage	lbs	solids lbs	solids lbs	solids lbs	solids lbs
time							
13:00	33919	21505	596	2123	1295	764	466
14:00	32640	34049	671	2898	1768	955	583
15:00	30720	32257	669	2234	1363	954	582
16:00	32640	32257	671	2426	1480	1337	816
17:00	32640	32257	745	3272	1996	763	465
18:00	32640	34049	670	1719	1049	1146	699
19:00	32640	32257	671	2275	1388	2292	1398
hourly							
average	32548	31233	670	2421	1477	1173	716
Line 1			344		758		367
Line 2			326		719		348

37990 =average lbs. per hour finished product produced during testing

326 =average lbs. per hour of MDI resin used during testing

0.86% = MDI resin used as % of finished product

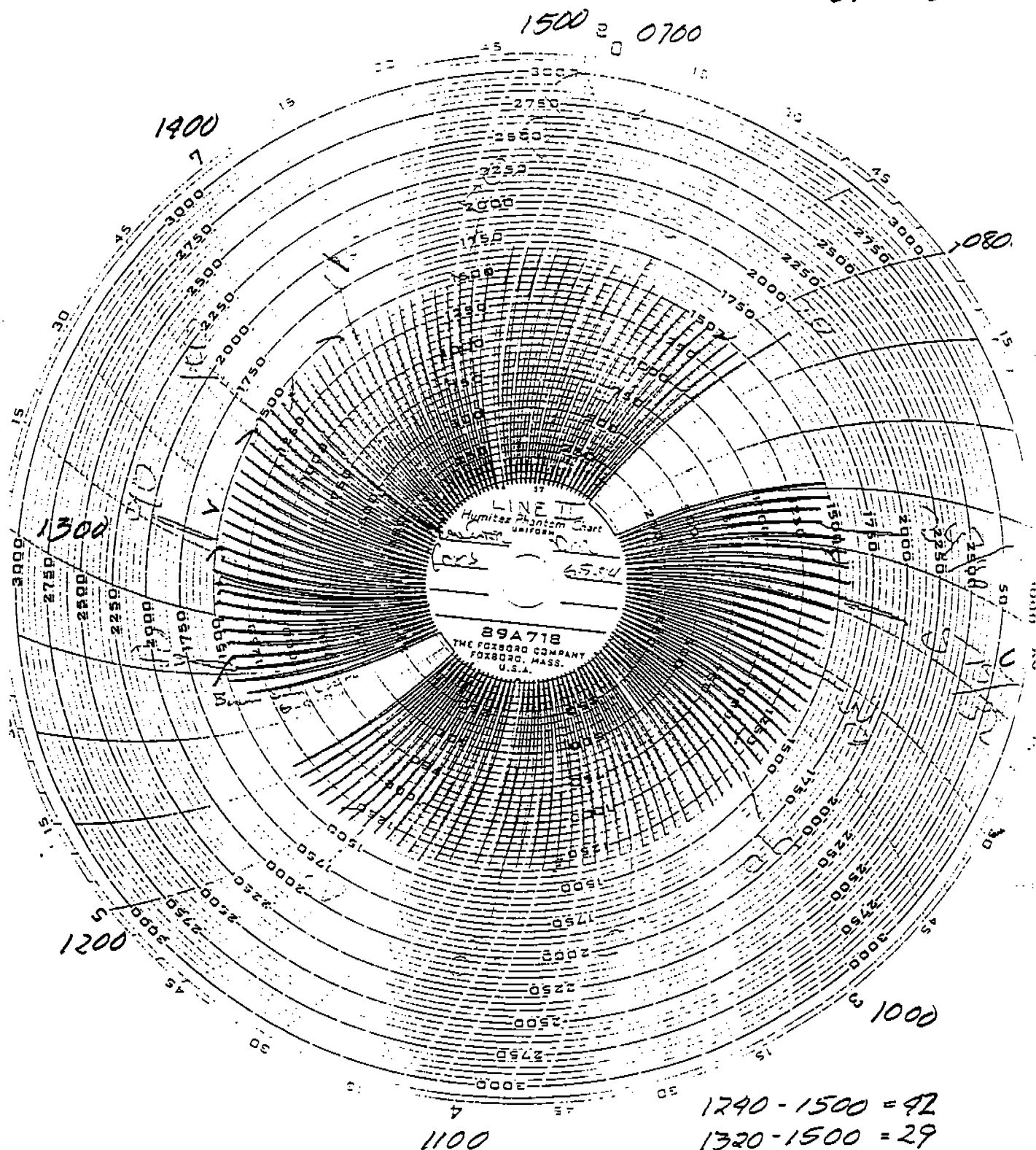
719 =average lbs. per hour of phenolic resin (100% solids) used during testing

1.89% =Phenolic resin used as % of finished product

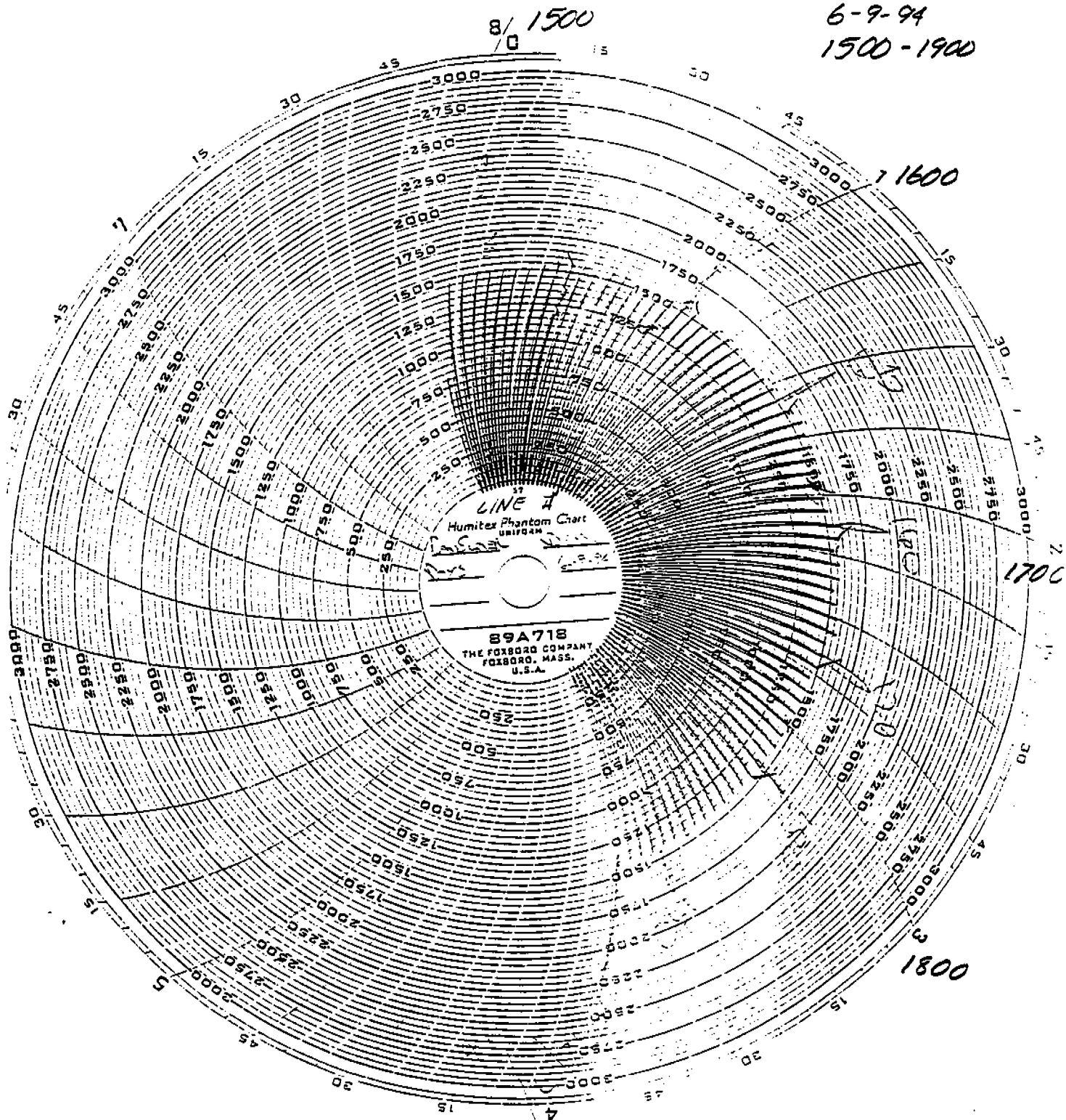
348 =average lbs. per hour of wax (100% solids) used during testing

0.92% =wax used as % of finished product

LINE II
PRESS CHA. 7
6-9-94
0700-1500



LINE 1
PRESS CHART
6-9-94
1500-1900



1500 - 1720 = 42
1500 - 1830 = 64

PRESS REPORT - LINE 2 *B/P*

PRESS LOADS 1947/6 5 1/32

DISPOSITION **17**

TOTAL HOURS:

LOG CODE: 7733

F.C.S. HAS RADIATOR 9:20

Cleaned Blender Strainer & Jar

Cleaned Deckle Cores

Printed Below Down 

Hardware Cleared	YES/NO	
------------------	--------	--

How Many

Former Hyd Radiator

LINE	SPEED	FROM	TO
61	7.00		
64	7.00		
58	8.50		15/32
64	9.07		7/16

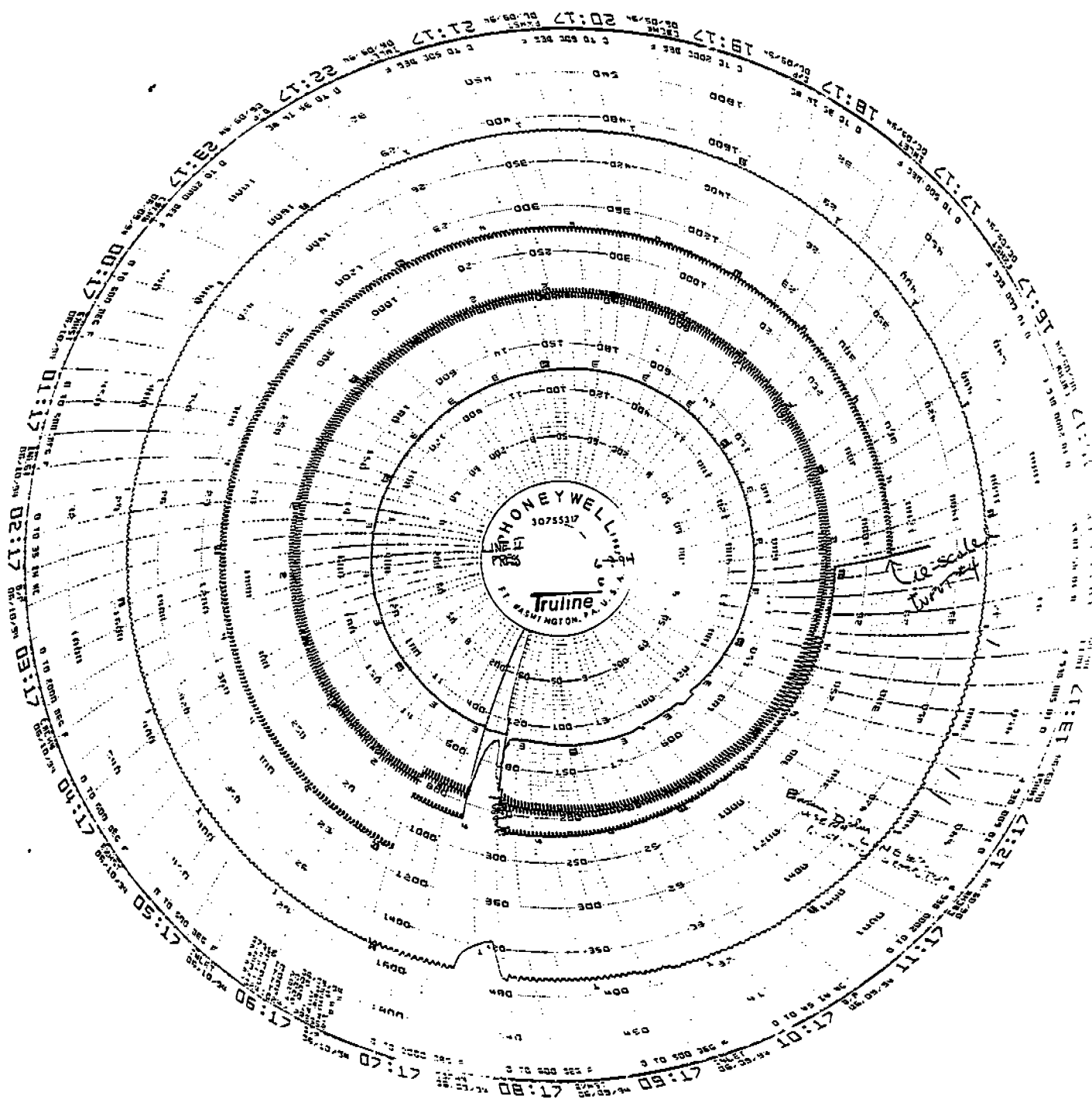
[illegible]

Downtime Code: X - Mechanical

I - General

Q - ~~Continuing~~

LINE II
DRESS RTO
CHART
6-9-94



LINE II PRESS - 6-9-94

182

#1	#2	#3	#4	#5	INLET PRESS.	BURNERS B #1 B #2	INLET TEMP.	COMBUST. CHAMBER TEMP.	EXHAUST TEMP.	A.P. AMP.	GAS
800	419	386	343	429	4.0	1577 1589	113	1522	224	19.1	020646
815	419	386	343	429	4.0	DOWN - STEAM					020648
830	419	386	343	429	4.0	DOWN					
845	440	411	342	436	3.9	1570 1593	116	1527	223	19.5	020650
900	429	403	348	432	4.0	1575 1568	115	1536	233	19.7	020652
915	428	400	345	431	4.3	1570 1586	116	1521	223	19.8	020654
930	428	396	349	429	4.1	1602 1599	118	1536	239	19.4	020656
945	423	394	348	430	4.1	1579 1575	117	1538	235	19.5	020658
1000	426	397	346	433	4.2	1566 1589	121	1532	226	19.8	020661
1015	430	398	349	434	4.3	1573 1589	118	1537	228	19.4	020663
1030	433	399	352	435	3.8	1579 1588	118	1541	233	19.2	020666
1045	430	399	357	436	4.0	1590 1584	120	1560	240	19.6	020668
1100	433	402	350	437	3.9	1570 1584	120	1546	232	19.6	020670
1115	432	405	359	438	3.9	1578 1585	119	1546	238	19.2	020673
1130	438	405	364	439	4.1	1595 1592	118	1552	246	19.6	020676
1145	438	406	366	442	4.2	1593 1586	117	1557	246	19.7	020678
1200	440	409	364	445	4.1	1573 1588	117	1547	231	19.5	020681
1215	445	410	369	443	4.0	1587 1590	119	1550	243	19.6	020683
1230	442	411	373	447	4.2	1592 1584	123	1558	249	19.6	020686
1245	446	414	375	449	4.0	1592 1572	117	1555	249	19.1	020688
1300	442	416	369	459	4.3	1558 1581	121	1538	235	19.5	020690
1315	450	417	372	450	3.6	1564 1581	120	1535	241	19.0	020693
1330	443	416	372	449	3.7	1580 1566	122	1552	247	19.4	020695
1400	451	419	373	448	3.8	1565 1581	121	1536	243	19.5	020697
2000	445	416	379	448	4.0	1593 1572	124	1552	252	19.1	020699
2100	450	421	373	450	4.3	1555 1576	122	1535	239	19.3	020702

LINE II PRESS 6-9-94

#1	#2	#3	#4	#5	INLET PRESS.	BURNERS B #1 B #2	INLET TEMP.	COMBUST. CHAMBER TEMP.	EXHAUST TEMP.	AP AMR.	GAS
23	478	413	390	412	4.1	1572 1572	123	1542	250	19.1	020724
24	478	415	386	415	4.1	1557 1569	124	1534	239	19.1	020725
25	456	418	386	447	4.0	1563 1565	123	1537	247	19.4	020708
26	486	421	384	450	4.2	1556 1569	124	1533	241	19.3	020711
27	453	421	388	450	3.9	1564 1563	123	1544	250	19.1	020713
28	456	425	388	451	4.0	1572 1566	125	1541	253	19.4	020715
29	456	424	388	451	4.1	1570 1571	124	1541	253	19.0	020717
30	457	426	386	452	4.0	1564 1571	125	1536	247	19.4	020720
31	453	426	386	454	4.0	1554 1564	124	1541	246	19.3	020722
32	454	425	388	453	4.2	1570 1564	124	1543	252	19.3	020724
33	457	426	388	452	3.8	1570 1569	125	1538	252	19.2	020726
34	458	427	385	453	3.8	1559 1569	124	1532	243	18.9	020729
35	455	427	385	453	3.8	1551 1566	125	1535	243	19.3	020731
36	455	427	386	453	3.8	1559 1559	134	1543	249	19.3	020733
37	457	428	387	451	4.0	1570 1569	125	1541	255	19.3	020736
38	460	428	385	450	3.9	1564 1571	125	1536	250	19.3	020738
39	458	430	382	450	4.1	1552 1568	124	1531	241	19.3	020740
40											
41											
42											
43											
44											
45											
46											
47											
48											
49											
50											

LINE 2 PRESS TESTING JUNE 10, 1994 - FORMALDEHYDE

DATA TIME: START= 08:10 END= 12:00 HOURS= 3.83
 START= 13:10 END= 13:40 HOURS= 0.50
 total 4.33

BOARD WEIGHTS - LBS

weights of approximately every 25th untrimmed board (from press tapes)
 7/16"

178	192	194	194
180	186	198	198
190	192	190	194
184	194	190	190
192	196	200	188
192	190	202	194
190	194	202	190
196	190	194	192
196	172	190	200
190	196	196	194
192	196	196	

191.93 lb=average
 untrimmed
 mat weight

176.77 lb=average
 finished board
 weight
 (untrimmed mat
 weight-weight
 of trim)

7.9% =trim %

PLANT PRODUCTION RATE

4.33 =hours during testing
 78 =pressloads
 936 =no. of 8'x16' boards produced (pressloads x12boards per load)
 165457 =lbs of finished product (boards produced x weight of finished board)
 38183 =lbs of finished product per hour (lbs of finished product / hours)
 19.09 =tons of finished product per hour (lbs of finished product per hour / 2000 lb)

Handwritten: 27.67 MSF / hr 7/16

RESIN USAGE FROM TANK MEASUREMENTS

Note: common tanks supply wax and resin to both Line 1 and Line 2. Usage for one line is estimated by proportioning the total usage by the footage (3/8" basis) for each line)

MEASUREMENT SUMMARY:

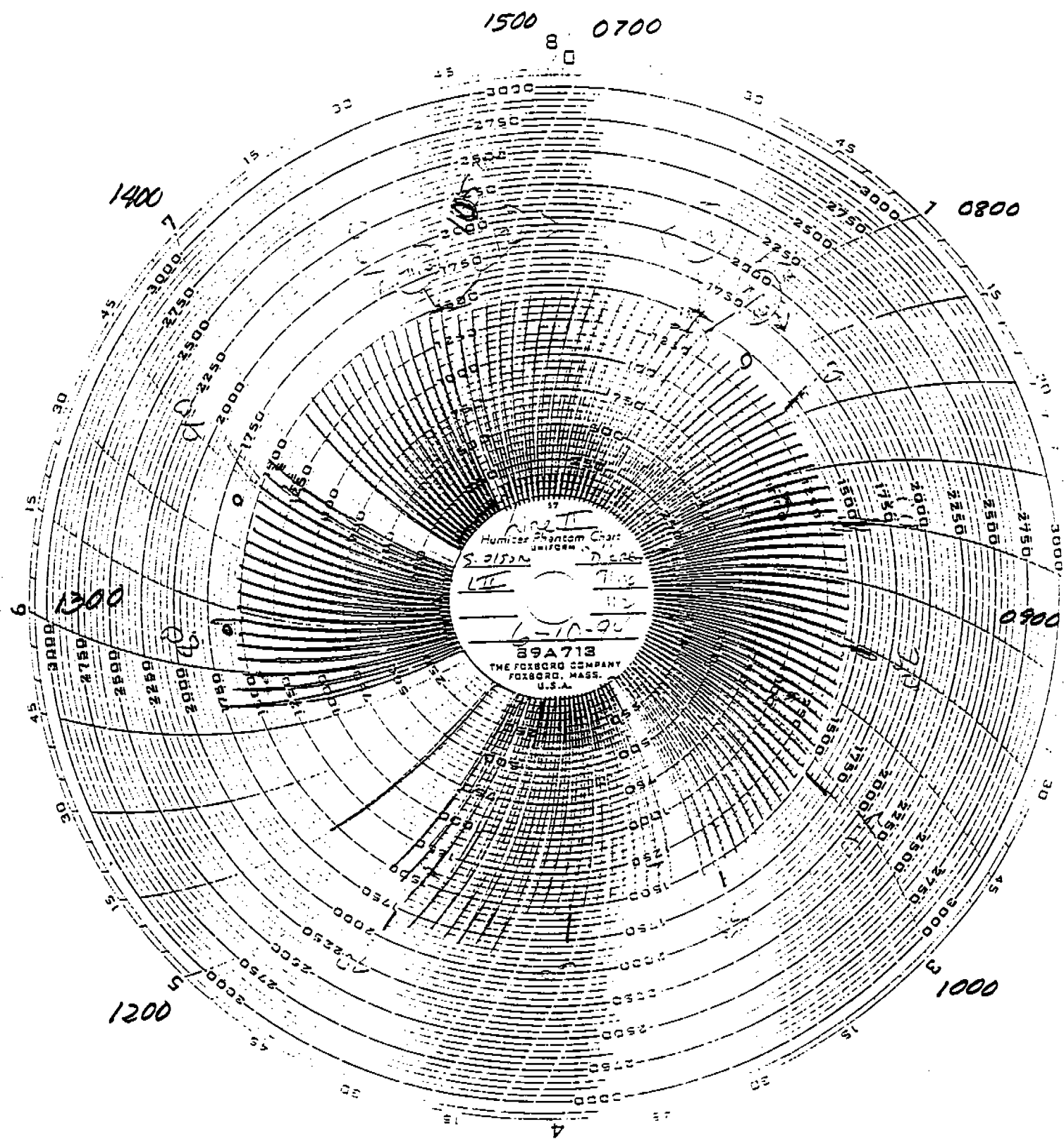
	line 1	line 2	MDI	PHENOLIC 61%	PHENOLIC 100%	WAX 58%	WAX 100%
	footage	footage	lbs	solids lbs	solids lbs	solids lbs	solids lbs
08:00	33536	32767	967	2376	1449	590	342
09:00	32257	30465	820	2376	1449	1527	886
10:00	28673	32257	521	2497	1523	764	443
11:00	32257	30465	522	2508	1530	764	443
12:00	34049	30465	745	2285	1394	1145	664
13:00	30465	8960	149	1436	876	382	222
14:00	28673	28673	669	2335	1424	1146	665
hourly							
average	31416	27722	628	2259	1378	903	523
Line 1			322		707		269
Line 2			305		671		255

38183 =average lbs. per hour finished product produced during testing
 305 =average lbs. per hour of MDI resin used during testing
 0.80% = MDI resin used as % of finished product

671 =average lbs. per hour of phenolic resin (100% solids) used during testing
 1.76% =Phenolic resin used as % of finished product

255 =average lbs. per hour of wax (100% solids) used during testing
 0.67% =wax used as % of finished product

LINE II
PRESS CHART
6-10-94



PRESS REPORT - LINE 11

LINE SPEED	FROM	TO
56	7:00	8:02
63	8:02	

PRESS LOADS 17 1/2
DECOMPRESSION TIME 10 / 2
TOTAL REPAIRS: _____
LOG COUNT: 7006
F.C.O.S. HYD RADIATOR ✓
Cleaned Blender Straps & Tracks ✓
Cleaned Ductile Cables ✓
Press Blows Down ✓
Headbars Cleaned YES/NO
How Many NONE
Former Hyd Radiator _____

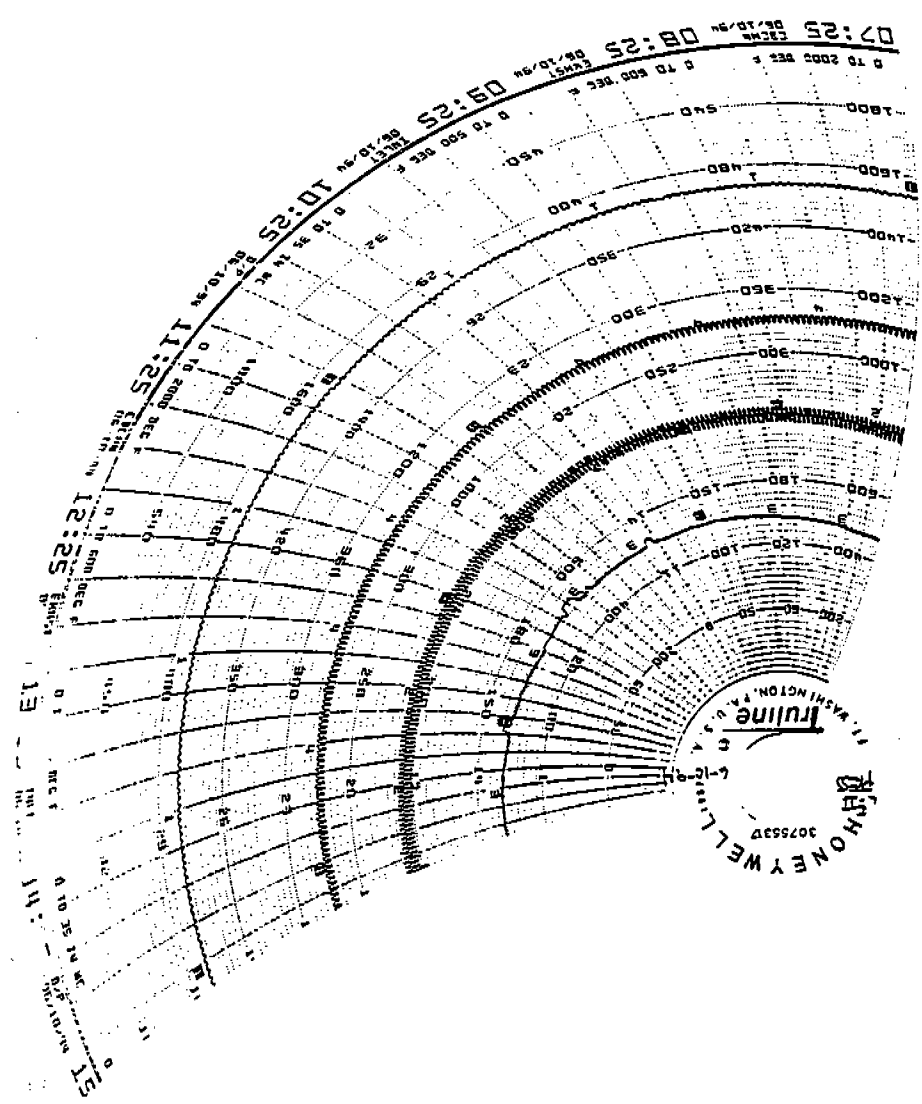
[illegible]

E - ~~Electrical~~
J-52

0 - Open End

51

52



07:25
08:25
09:25
10:25
11:25
12:25
0 10 2000 DEC
0 10 500 DEC
0 10 100 DEC
0 10 50 DEC
0 10 20 DEC
0 10 10 DEC
0 10 5 DEC
0 10 2 DEC
0 10 1 DEC
0 10 0.5 DEC
0 10 0.2 DEC
0 10 0.1 DEC

LIVE II
PRESS RTO
CHART
6-10-94

6/10/92 NJ

#1	#2	#3	#4	#5	INLET PRESS.	BURNERS B #1 B #2	INLET TEMP.	COMBUST. CHAMBER TEMP.	EXHAUST TEMP.	AMP.	GAS
300	445	412	373	457	3.8	1562 1563	116	1542	242	19.6	020861
315	446	412	374	456	4.2	1569 1565	117	1542	244	19.5	020863
330	449	413	375	456	4.0	1569 1573	117	1539	248	19.1	020866
345	452	414	375	457	3.7	1571 1565	117	1535	247	19.2	020868
360	452	415	375	458	3.7	1563 1566	119	1531	239	19.0	020870
375	450	416	374	461	4.0	1553 1568	119	1530	235	19.4	020873
390	449	416	376	460	3.8	1553 1563	120	1537	240	19.4	020875
405	448	416	380	460	3.9	1564 1563	121	1544	244	19.2	020877
420	452	417	382	458	4.0	1569 1568	121	1540	252	19.4	020879
435	475	418	381	459	3.9	1567 1566	123	1537	247	18.9	020881
450	475	421	380	459	4.1	1559 1568	122	1531	238	19.3	020884
465	453	421	381	459	3.9	1552 1565	122	1532	241	19.4	020886
480	450	420	381	459	3.9	1570 1566	122	1538	253	19.3	020888
495	455	421	385	457	3.8	1565 1569	123	1534	246	19.0	020891
510	455	423	383	457	3.8	1565 1569	123	1532	239	19.0	020893
525	453	424	381	456	4.0	1554 1569	124	1532	252	18.9	020895
540	454	422	385	455	4.0	1568 1565	123	1540	252	19.3	020897
555	453	423	385	454	4.0	1566 1566	124	1540	253	17.1	020899
570	457	425	385	453	3.7	1566 1566	130	1535	243	19.0	020902
585	457	429	384	454	4.0	1554 1569	125	1532	245	19.3	020904
600	456	430	384	453	3.9	1551 1563	124	1538	245	19.0	020907
615	457	431	383	451	4.1	1557 1568	124	1531	241	19.0	020909
630	454	430	386	448	3.9	1560 1561	124	1540	250	19.3	020911
645	458	432	384	447	3.6	1560 1569	126	1535	244	19.3	020914
660	454	432	383	447	3.8	1552 1569	123	1537	241	19.3	020914

532 244

MONUS DATA READINGS EVERY 10 MINUTES PLANT

DATE 6-7-93 PAGE 1 OF 2

BY

1 count = 10 lb

TIME	K1			K2			K3			K4			FUEL COUNT		ONCE/HR BARK MOISTURE
	OIL IN TEMP	OIL OUT TEMP	I.D. FAN W.C	OIL IN TEMP	OIL OUT TEMP	I.D. FAN W.C	OIL IN TEMP	OIL OUT TEMP	I.D. FAN W.C	OIL IN TEMP	OIL OUT TEMP	I.D. FAN W.C	K1	K2	
0800				239	256	7	239	252	7	239	252	7	399	88	
0810				252	260	7	252	260	7	244	260	7	401	93	
0820				236	260	7	236	260	7	253	265	4	403	93	
0830				230	250	6.5	230	250	6.5	234	244	4	480	99	
0840				230	252	7	230	252	7	236	251	4	499	110	
0850				232	255	7	232	255	7	238	253	4	543	120	
0900				243	260	7	243	260	7	238	253	4	592	131	
0910				234	260	7	234	260	7	245	257	4	601	133	
0920				237	260	7	237	260	7	238	250	4	645	140	
0930				233	255	7	233	255	7	238	254	4	696	152	
0940				239	260	7	239	260	7	244	257	4	719	153	
0950				238	260	7	238	260	7	242	253	4	729	160	
1000				236	255	7	236	255	7	239	253	4	713	172	
1010				235	260	7	235	260	7	241	256	4	804	180	
1020				235	256	7	235	256	7	239	250	4	867	185	
1030				234	255	7	234	255	7	241	255	4	894	197	
1040				234	256	7	234	256	7	240	254	4	943	208	
1050				237	252	7	237	252	7	235	249	4	990	222	
1100				232	252	7	232	252	7	236	261	4	1039	235	
1110				233	255	7	233	255	7	239	256	4	1086	246	
1120				234	257	6.5	234	257	6.5	238	253	4	1133	253	
1130				240	260	6.5	240	260	6.5	242	251	4	1146	259	
1140				235	259	6.5	235	259	6.5	239	252	4.5	1163	263	
1150				236	260	6.5	236	260	6.5	244	253	4.5	1171	275	
1200				235	260	6	235	260	6	240	257	4.5	1208	284	
1210				235	260	6.5	235	260	6.5	241	253	4	1233	293	
1220				237	261	6	237	261	6	246	257	4	1233	297	
1230				239	265	6.5	239	265	6.5	242	255	4	1233	298	
1240				235	257	6.5	235	257	6.5	241	252	4	1247	307	
1250				236	260	6.5	236	260	6.5	239	254	4	1300	318	

KONUS DATA READINGS EVERY 10 MINUTES

PLANT *Hayward*

BY _____

DATE *6-7-9* PAGE *2* OF *2*

TIME	K1			K2			K3			K4			FUEL COUNT				ONCE/HR BARK MOISTURE
	OIL IN TEMP	OIL OUT TEMP	I.D. FAN W/G	OIL IN TEMP	OIL OUT TEMP	I.D. FAN W/G	OIL IN TEMP	OIL OUT TEMP	I.D. FAN W/G	OIL IN TEMP	OIL OUT TEMP	I.D. FAN W/G	K1	K2	K3	K4	
1300							238	262	6.5	240	256	4			1328	323	
1310							253	265	6	242	250	4			1328	323	
1320							256	271	6	254	260	4.5			1329	323	
1330							271	270	4	246	258	4.5			1329	323	
1340							240	270	6	245	254	4.1			1329	327	
1350							253	265	6	249	257	4.5			1329	333	
1400							255	265	6.5	252	260	6			1329	333	
1410							260	270	6.5	256	267	6			1329	333	
1420							262	272	6.5	254	270	5.5			1329	333	
1430							260	270	6.5	255	268	6			1329	333	
1440							251	260	4	247	260	6			1331	333	
1450							232	255	7	239	249	5			1364	335	
1500							232	255	6	237	237	5			1407	346	
1510							236	245	7	234	242	5			1453	357	
1520							235	245	7	230	240	4.7			1504	370	
1530							235	245	7	234	242	5			1505	381	
1540							235	245	7	235	236	4.5			1599	393	
1550							236	245	7	234	246	4.5			1646	407	
1600							236	245	7	237	246	4.5			1709	421	
1610							239	250	7	242	250	4.5			1766	434	
1620							232	255	7	237	255	4.5			1828	447	
1630							235	260	7	244	255	4.0			1863	457	
1640							241	260	7	242	252	4.0			1901	468	
1650							234	260	8	241	255	3.5			1924	470	
1700							238	259	8.2	242	259	2.5			1950	478	
1710																	
1720																	
1730																	
1740																	
1750																	

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KONUS DATA READINGS EVERY 10 MINUTES

BY

DATE 6-8-94

PAGE 1

OF 1

PLANT Hayward

TIME	K1			K2			K3			K4			FUEL COUNT			ONCE/HR BARK MOISTURE	
	OIL IN TEMP	OIL OUT TEMP	ID. FAN W.C.	OIL IN TEMP	OIL OUT TEMP	ID. FAN W.C.	OIL IN TEMP	OIL OUT TEMP	ID. FAN W.C.	OIL IN TEMP	OIL OUT TEMP	ID. FAN W.C.	K1	K2	K3	K4	
0800	245	240	1.5	256	250	3.2	226	240	9	235	241	2	200	176	162	44	
0810	240	255	1.5	224	258	3.2	226	245	9	234	238	2	205	194	191	54	
0820	245	255	1.5	227	256	3.2	226	245	9	236	241	3	225	217	225	64	
0830	245	260	1.6	229	257	3.1	225	245	9	235	241	3	235	266	254	79	
0840	243	255	1.3	227	253	1.2	227	249	9	238	246	3.5	257	271	278	97	
0850	244	257	1.5	227	251	1.3	226	248	9	241	250	3.5	278	294	336	104	
0900	245	256	1.5	229	250	1.2	227	245	9	241	251	2.5	291	317	372	117	
0910	246	255	1.4	230	253	1.0	229	247	9	243	253	3	299	326	407	130	
0920	244	254	1.8	227	254	1.1	232	250	9	247	256	3	321	354	448	137	
0930	241	250	1.5	225	253	1.6	243	255	9	252	261	2.5	340	396	472	138	
0940	239	246	1.6	223	255	1.3	238	260	9	252	260	3	362	443	506	138	
0950	239	249	1.8	223	256	1.2	236	259	9	257	261	3	386	476	517	138	
1000	238	245	1.4	221	249	1.1	241	260	9	248	255	3	405	510	550	140	
1010	237	246	1.6	221	254	1.4	230	250	9	246	255	3	423	549	570	140	
1020	237	245	1.4	221	256	1.3	236	250	9	240	249	2.5	449	582	613	157	
1030	237	244	1.4	221	257	1.1	232	252	9	241	249	2.5	467	603	644	163	
1040	236	242	1.4	221	257	1.2	231	251	9	240	248	2	489	616	681	176	
1050	237	244	1.4	226	250	1.6	232	253	9	240	245	2.5	514	673	725	192	
1100	239	249	1.3	224	256	1.2	231	255	9	242	251	2.5	533	697	757	204	
1110	241	249	1.5	225	249	1.6	231	250	9	242	255	2.5	557	714	747	219	
1120	239	249	1.6	224	255	1.3	232	251	9	242	256	2.5	576	747	839	229	
1130	239	249	1.6	224	254	0	237	256	8.5	241	255	2.5	599	762	869	236	
1140	240	250	1.6	226	253	1.7	241	258	9	244	257	2.5	629	786	904	238	
1150	244	250	1.4	230	256	1.3	237	260	9	251	257	3	643	798	923	238	
1200	240	251	1.3	225	255	1	244	260	9	250	258	3	662	822	929	238	
1210	240	252	1.4	228	256	1.3	237	260	9	247	255	3	689	853	941	238	
1220	240	249	1.5	225	256	1.3	238	259	9	248	256	3	710	889	963	241	
1230	240	249	1.3	225	253	1.5	238	260	8.5	244	254	2.5	727	909	992	249	
1240	235	240	1.9	218	234	1	236	260	9.5	247	256	3	751	909	1032	253	
1250	225	235	1.9	210	228	1.5	239	257	6.5	249	255	3	771	909	1057	253	

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KONUS DATA PLANT *Forward*

READINGS EVERY 10 MINUTES

BY _____

DATE *6-8-94* PAGE *2* OF *4*

TIME	K1			K2			K3			K4			FUEL COUNT				ONCE/HR BARK MOISTURE
	OIL IN TEMP	OIL OUT TEMP	ID. FAN W/G	OIL IN TEMP	OIL OUT TEMP	ID. FAN W/G	OIL IN TEMP	OIL OUT TEMP	ID. FAN W/G	OIL IN TEMP	OIL OUT TEMP	ID. FAN W/G	K1	K2	K3	K4	
1300	229	239	-1.6	209	238	-2.5	237	262	8	243	253	2.5	782	959	1084	140	
1310	226	239	-1.6	211	244	-2.1	240	259	8.5	243	254	2.5	906	1016	1113	370	
1320	227	230	-1.8	212	242	-2.9	236	260	8.5	243	253	3	825	1036	1139	282	
1330	225	220	-1.6	210	228	-3.1	236	255	8.5	237	252	2.8	852	1044	1161	277	
1340	225	226	-1.6	208	238	-2.4	231	257	8.5	239	254	3	868	1053	1184	305	
1350	225	227	-1.8	209	243	-2.2	234	257	9	241	253	2.5	896	1143	1201	321	
1400	229	235	-1.6	213	247	-2.8	235	260	9	244	255	2	918	1174	1210	329	
1410	230	230	-1.3	214	230	-3.4	253	261	9	246	255	2	958	1174	1237	357	
1420	230	247	-1.4	212	225	-3.2	239	265	8.5	251	259	3	986	1174	1239	337	
1430	232	251	-1.4	216	223	-3.2	244	265	9	243	255	2.5	1006	1170	1248	340	
1440	246	251	-1.5	220	229	-3.1	240	270	9	232	245	3	1013	1174	1252	341	
1450	237	256	-1.5	220	229	-3.1	237	266	9	235	242	3	1033	1174	1252	342	
1500	239	255	-1.2	221	239	-3.1	240	259	9	231	241	2	1050	1174	1252	342	
1510	241	260	-1.3	226	240	-3.1	226	245	9	225	236	3	1060	1197	1268	342	
1520	243	257	-1.6	228	246	-3.2	224	239	9	224	234	2	1080	1219	1303	356	
1530	246	252	-1.6	231	249	-3.1	224	240	9	227	238	2	1083	1234	1346	372	
1540	244	255	-1.5	229	250	-3.2	224	240	9	227	248	2	1100	1243	1377	375	
1550	240	247	-1.6	222	246	-3.2	226	241	9	226	248	2.5	1120	1240	1415	380	
1600	235	243	-1.5	220	245	-3.2	228	245	9	240	251	3	1125	1243	1451	394	
1610	237	252	-1.5	221	245	-3.2	230	246	9	241	261	2.5	1167	1284	1480	395	
1620	236	248	-1.5	223	247	-3.3	232	250	9	244	252	2.5	1181	1303	1528	395	
1630	235	245	-1.5	220	245	-3.1	232	250	9	245	253	3	1203	1319	1570	395	
1640	235	241	-1.4	219	243	-3.2	232	250	9	244	251	3	1217	1329	1586	395	
1650	235	229	-1.6	217	242	-3.1	235	255	9	249	254	3	1240	1345	1637	395	
16100	238	236	-1.6	216	243	-3.1	241	257	8	249	253	3	1258	1358	1673	395	
1710	231	240	-1.7	216	239	-3.1	240	260	9	250	256	3	1285	1374	1682	395	
1720	230	235	-1.6	214	237	-3.1	240	260	8	250	257	3	1301	1389	1682	395	
1730	229	235	-1.7	213	234	-3.1	245	257	8.5	250	259	3	1322	1406	1692	395	
1740	227	235	-1.7	211	232	-3.2	240	260	8	252	258	3	1342	1423	1712	395	
1750	225	234	-1.7	209	228	-3.1	241	265	8	254	263	2	1355	1443	1730	395	

KONUS DATA HEADINGS EVERY 10 MINUTES

DATE 6-8-74 PAGE 3 OF 1

BY

PLANT

Hayward

TIME	K1			K2			K3			K4			FUEL COUNT			ONCE/HR BARK MOISTURE	
	OIL IN TEMP	OIL OUT TEMP	ID. FAN W.C.	OIL IN TEMP	OIL OUT TEMP	ID. FAN W.C.	OIL IN TEMP	OIL OUT TEMP	ID. FAN W.C.	OIL IN TEMP	OIL OUT TEMP	ID. FAN W.C.	K1	K2	K3	K4	
1800	221	227	-1.4	204	220	3.1	216	268	5	254	261	2	1371	1470	1741	395	
1810	220	225	-1.6	201	220	3.1	211	261	7	249	263	5.5	1396	1520	1753	395	
1820	227	227	-1.6	211	235	3.1	235	251	7	241	254	5.5	1412	1568	1771	395	
1830	232	237	-1.8	218	247	2.2	237	258	7	233	245	5	1434	1619	1811	401	
1840	228	241	-1.7	223	253	3.2	229	248	7	229	240	5	1439	1626	1890	445	
1850	241	246	-1.6	227	254	3.2	227	245	7	233	243	5	1459	1651	1826	420	
1900	235	239	-1.4	219	243	3.2	229	245	7	240	241	6	1481	1674	1896	436	
1910	235	240	-1.6	219	248	3.2	230	247	7	211	253	6	1503	1706	1929	438	
1920	237	246	-1.6	221	253	3.1	232	250	7	245	254	6	1522	1736	1966	438	
1930	247	257	-1.5	229	259	3.1	234	250	7	245	255	6	1542	1759	2004	438	1765
1940	242	254	-1.5	232	262	2.7	236	255	7	251	261	6	1562	1794	2029	438	
1950																	
2000																	
2010																	
2020																	
2030																	
2040																	
2050																	
2100																	
2110																	
2120																	
2130																	
2140																	
2150																	
2200																	
2210																	
2220																	
2230																	
2240																	
2250																	

KONUS DATA
PLANT _____

KONUS DATA
PLANT _____

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DATE_

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[illegible]

KONUS DATA READINGS EVERY 10 MINUTES PLANT Hayward

DATE 6-9-91 PAGE 7 OF 7

BY

TIME	K1			K2			K3			K4			FUEL COURT			ONCEHR	
	OIL IN TEMP	OIL OUT TEMP	ID. FAN W.C	OIL IN TEMP	OIL OUT TEMP	ID. FAN W.C	OIL IN TEMP	OIL OUT TEMP	ID. FAN W.C	OIL IN TEMP	OIL OUT TEMP	ID. FAN W.C	K1	K2	K3	K4	BARK MOISTURE
840	231	240	-1.5	216	240	3.1							211	149			
850	230	238	-1.5	215	234	-3.2							236	160			
900	230	237	-1.6	214	233	3.2							246	176			
910	230	235	-1.6	214	240	-3.7							263	190			
920	230	236	-1.5	214	233	-3.3							282	205			
930	227	236	-1.7	212	228	-3.2							300	220			
940	226	235	-1.5	210	228	-3.2							319	230			
950	225	235	-1.5	208	227	-3.1							340	248			
96 JUNE	225	237	-1.4	206	221	-3.1							355	257			
1000	225	235	-1.4	208	228	-3.1							375	280			
1020	226	235	-1.4	211	234	3.2							374	303			
1030	227	235	-1.4	211	236	3.1							412	326			
1040	227	235	-1.5	211	229	-3.2							430	357			
1050	225	234	-1.4	208	223	-3.1							448	375			
1100	223	231	-1.5	207	229	3.1							469	405			
1110	224	230	-1.5	209	231	-3.2							487	432			
1120	226	230	-1.6	210	232	-3.1							506	451			
1130	222	230	-1.6	205	216	2.7							523	451			
1140	224	229	-1.5	205	215	-3.1							547	453			
1150	225	230	-1.5	208	222	-3.2							581	492			
1200	229	235	-1.5	213	232	3.1							611	508			
1210	229	237	-1.6	216	245	3.8							642	535			
1220	222	235	-1.5	215	248	-3.1							656	557			
1230	229	235	-1.5	213	227	-3.2							671	559			
1240	225	231	-1.6	211	231	-3.1							687	577			
1250	226	232	-1.6	210	228	3.1							702	588			

KONUS DATA

READINGS EVERY 10 MINUTES

PLANT *1/2*

DATE *6/1/74* PAGE *1* OF *1*

BY *1/2*

TIME	K1			K2			K3			K4			FUEL			ONCE AIR	
	OIL IN TEMP	OIL OUT TEMP	I.D. FAN W.C.	OIL IN TEMP	OIL OUT TEMP	I.D. FAN W.C.	OIL IN TEMP	OIL OUT TEMP	I.D. FAN W.C.	OIL IN TEMP	OIL OUT TEMP	I.D. FAN W.C.	K1	K2	K3	K4	BARK MOISTURE
1300	224	231	1.5	227	229	3.1							719	608			
1310	234	231	1.5	207	225	3.1							733	611			
1320	225	232	1.4	207	223	3.2							748	629			
1330	225	236	1.4	210	220	3.0							712	641			
1340	227	235	1.5	212	220	3.0							778	665			
1350	230	235	1.5	214	236	3.2							793	679			
1400	227	239	1.4	213	236	3.2							808	696			
1410	220	240	1.4	214	235	3.2							825	716			
1420	220	240	1.4	213	227	3.2							839	720			
1430	231	241	1.3	216	226	3.2							855	720			
1440	232	244	1.3	217	227	3.2							869	720			
1450	231	244	1.4	216	223	3.2							884	720			
1500	234	249	1.5	218	227	3.1							900	739			
1510	231	242	1.4	216	233	3.2							914	756			
1520	225	235	1.4	211	230	3.1							930	779			
1530	220	235	1.4	210	225	3.1							945	795			
1540	225	235	1.4	207	231	3.2							961	814			
1550	225	233	1.5	209	235	3.2							975	831			
1600	225	234	1.5	210	231	3.2							991	851			
1610	225	232	1.5	208	229	3.2							1007	865			
1620	223	231	1.5	207	225	3.2							1021	886			
1630	221	231	1.4	205	221	3.2							1037	908			
1640	222	230	1.4	205	227	3.2							1055	934			
1650	222	229	1.4	205	231	3.2							1073	956			
1700	225	230	1.5	208	235	3.2							1095	982			
1710	226	236	1.4	211	238	3							1119	1001			
1720	229	240	1.4	214	242	3							1136	1020			
1730	232	245	1.4	218	245	3							1158	1036			
1740	235	245	1.3	221	250	3.0							1160	1048			
1750	232	245	1.3	219	246	2.9							1173	1060			

KONUS DATA READINGS EVERY 10 MINUTES PLANT *Highland, W. 30 mi S/A*

DATE *6/1/74* PAGE *62*

TIME	K1			K2			K3			K4			FUEL COUNT			ONCE/HR BARK MOISTURE
	OIL IN TEMP	OIL OUT TEMP	I.D. FAN W.C	OIL IN TEMP	OIL OUT TEMP	I.D. FAN W.C	OIL IN TEMP	OIL OUT TEMP	I.D. FAN W.C	OIL IN TEMP	OIL OUT TEMP	I.D. FAN W.C	K1	K2	K3	
1800	234	249	1.3	220	245	2.8							1185	1073		
1810	235	248	1.4	220	247	3.2							1191	1084		
1820	236	249	1.3	221	247	3.2							1206	1097		
1830	235	248	1.3	220	243	3.2							1221	1110		
1840	234	248	1.4	220	242	3.2							1233	1122		
1850	233	242	1.4	218	239	3.2							1247	1136		
1900	232	242	1.4	217	239	3.1							1262	1155		
1910																
1920																
1930																
1940																
1950																
2000																
2010																
2020																
2030																
2040																
2050																
2100																
2110																
2120																
2130																
2140																
2150																
2200																
2210																
2220																
2230																
2240																
2250																

EFB READINGS

DATE 6-7-94

BY JC

PLANT: HAYWARD K3 & K4

SOURCE: _____

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readings every 10 minutes

TIME	"A" SIDE				"B" SIDE <u>K3 & K4</u>				EFB PRESS.	BAG H. PRESS.
	BED VOLT	BED CURR.	ION VOLT	ION CURR.	BED VOLT	BED CURR.	ION VOLT	ION CURR.		
					13	0.05	22	2	2	5.5
0710					1					
0800					13	.04	22	2	2	5.7
0800					13	.04	22	2	2	5.7
0810					13	.08	22	2	2.2	5.6
0820					13	.08	22	2	1.8	5.6
0830					13	.08	22	2	2	5.6
0840					13	.09	22	2	1.8	5.6
0850					13	.09	22	1.9	2.2	5.6
0900					13	.1	22	1.9	2	5.6
0910					13	.1	27	4	2	5.6
0920					13	.1	23	2	2	5.6
0930					13	.1	23	2	1.8	5.8
0940					13	.1	23	2	2.2	5.8
0950					13	.1	23	2	2.0	6.0
1000					13	.1	25	2.8	2.2	6.0
1010					13	.1	22	1.8	2	6
1020					13	.1	22	1.8	2	6
1030					13	.1	23	1.8	2.2	6.2
1040					12	.1	22	1.8	1.8	6.2
1050					12	.1	22	1.8	2.2	6.2
1100					12	.1	22	1.8	1.9	6.2
1110					12	.11	22	1.8	2	6.2
1120					11.5	.11	22	1.8	1.8	6.2
1130					12	.11	22	1.8	2	6.2
1140					12	.1	22	1.8	2	5.7
1150					12	.1	22	1.8	1.8	5.6

EFB READINGS

DATE 6-7-94

BY JC
283

PLANT: Hayward K3 & K4

SOURCE:

readings every 10 minutes

TIME	"A" SIDE				"B" SIDE				EFB PRESS.	BAG H. PRESS.
	BED VOLT	BED CURR.	ION VOLT	ION CURR.	BED VOLT	BED CURR.	ION VOLT	ION CURR.		
1200					12	22 12	22	1.8	5.2	5.6
1210					12	.12	22	1.8	1.8	5.8
1220					11.5	.12	22	1.8	2	5.8
1230					12	.12	22	1.8	2.2	5.8
1240					11.5	.12	22	1.8	2	5.4
1250					10.5	.10	22	1.8	2.2	5.8
1300					10.5	.10	22	1.8	1.6	5.8
1310					11	.10	22	1.8	1.9	6.0
1320					11	.1	22	1.8	2.3	6.0
1330					11	.1	22	1.8	2	6
1340					11	.1	22	1.8	2	6
1350					11	.1	21.5	1.6	1.9	6
1400					11.5	.1	22	1.6	1.8	6
1410					12	.1	22	1.6	1.5	6
1420					12	.1	22	1.6	2.1	6
1430					10.5	.08	23.5	2.2	1.8	6.2
1440					10.5	.08	24	2.2	2	6
1450					11	.08	23.5	2.2	2.4	6.2
1500					10.5	.08	23	2.2	2.6	6.2
1510					11	.08	21	1.6	2.2	6.2
1520					11	.07	21	1.6	2.2	6.1
1530					11	.07	22	1.6	2.2	6.1
1540					11	.08	22	1.6	1.7	6.1
1550					11	.08	22	1.6	2	6
1600					11	.07	22	1.6	1.7	6.1
1610					11	.07	21.5	1.6	2	6.1
1620					10.5	.08	22	1.6	2	6.2
1630					10.5	.08	22	1.6	1.4	6.2
1640					10.5	.08	22	1.6	1.6	6.2
1650					10.5	.08	22	1.5	1	6.1

EFB READINGS

DATE 6-7-94

BY JC

PLANT: Hayward K-3 & K-4

SOURCE: _____

303

readings every 10 minutes

TIME	"A" SIDE				"B" SIDE				EFB PRESS.	BAG H. PRESS.
	BED VOLT	BED CURR.	ION VOLT	ION CURR.	BED VOLT	BED CURR.	ION VOLT	ION CURR.		
1700					12	.1	22	1.6	1.2	6.4
1710										
1720										
1730										
1740										
1750										
1800										
1810										
1820										
1830										
1840										
1850										
1900										
1910										
1920										
1930										
1940										
1950										
2000										
2010										
2020										
2030										
2040										
2050										
2100										
2110										
2120										
2130										
2140										
2150										

EFB READINGS

DATE 6-8-94

BY JC

PLANT: Hayward K1, K2, K3, K4

1063

SOURCE:

readings every 10 minutes

TIME	"A" SIDE				"B" SIDE				EFB PRESS.	BAG H. PRESS.
	BED VOLT	BED CURR.	ION VOLT	ION CURR.	BED VOLT	BED CURR.	ION VOLT	ION CURR.		
0800	14	.03	21	.12	13	.08	21	1.2	1.5/1.5	3.3/5
0810	14	.03	21	.14	13	.08	21	1.2	1.7/1.3	3.2/5
0820	14	.04	22	.16	13	.08	21	1.2	1.7/1.8	3.2/5.1
0830	14	.04	22	1.7	13	.08	21	1.2	1.7/1.4	6/4.9
0840	13.5	.04	22	1.6	13	.09	21.5	1.2	1.9/1.1	6/4.9
0850	13	.04	22	1.6	13	.09	21.0	1.2	1.8/1.2	2/5
0900	12.5	.04	22	1.6	12.5	.09	21	1.2	1.8/1	2/5
0910	15	.04	22	1.8	12	.09	21	1.2	1.6/1.4	2.3/5
0920	15.8	.04	22	1.8	12.5	.09	21	1.2	1.4/1	2/5.2
0930	17	.05	26	2.8	12.5	.1	22	1.7	1.7/1.4	2.5/5.1
0940	16.17	.04	26	2.7	12.5	.09	23	1.8	1.5/1.4	2.8/5
0950	17.2	.04	26	2.9	12.5	.09	24	1.8	1.8/1.2	2.9/5
1000	17.5	.04	26	2.6	12.5	.09	23	1.8	1.9/.9	2.8/5
1010	15.5	.04	22	1.5	12	.08	23	1.8	1.8/1.2	2.9/5.2
1020	15.5	.04	22	1.4	12.5	.08	23	1.8	1.8/1.2	2.9/5.1
1030	16.5	.04	24	.7	12.5	.09	23	1.8	.3/1.2	3/5.1
1040	17.2	.02	24	.6	12.5	.09	23	1.8	.2/1	3/5
1050	16.5	.02	0	0	12.5	.09	23	1.8	.3/1.3	0/5.2
1100	14.5	.04	19.5	1	12	.1	23	1.8	1.5/1	3/5.2
1110	16	.03	19	1.1	11.7	.1	23	1.8	2/1	2.8/5.2
1120	15	.04	19	1.1	11.7	.1	23	1.8	2/1.04	2.5/5.3
1130	14	.04	19	1.1	11.5	.1	23	1.8	2.2/1.8	3.2/5.4
1140	14	.04	19	1.0	12	.10	23	1.8	2.2/1.4	3.1/5.5
1150	13.5	.04	19	1.0	12	.10	23.5	1.8	2.1/1.8	3/5.5
1200	13.2	.06	19	1.1	11.5	.1	24	1.8	2.2/1.4	3.2/5.5
1210	15.5	.06	19	1	12	.1	24	1.8	2.1/1.3	3.1/5.6
1220	15	.06	19	1	11.6	.1	24.5	1.8	2/1.9	3/5.4
1230	15	.06	19	1	11.5	.1	23	1.7	2.5/1.6	2.4/5.6
1240	15	.06	22	2	11.5	.1	24	1.9	2.6/1	3.4/5.6
1250	15.5	.07	23	2	12	.1	24	2	2.8/1	3.2/5.6

EFB READINGS

DATE 6-8-94

PLANT Hayward

BY J.C.

SOURCE: _____

243
readings every 10 minutes

TIME	"A" SIDE				"B" SIDE				EFB	
	BED VOLT	BED CURR.	ION VOLT	ION CURR.	BED VOLT	BED CURR.	ION VOLT	ION CURR.	PRESS.	BAG H. PRESS.
1300	15	.06	23	1.8	11.5	.1	24	2	2.5/1.6	3.4/5.5
1310	15	.06	23	1.9	12	.1	24	2	2.5/1.4	3.6/5.5
1320	16	.06	23	2	12	.1	24	2	2.5/1.6	3.5/5.8
1330	16.5	.06	22	2	12	.1	24	2	2.5/1.4	3.3/5.8
1340	16	.05	23	2	11.5	.12	24	2	2.4/1.8	3.6/5.1
1350	16	.05	23	1.9	12	.1	24	2	2.5/1.1	2.4/5.7
1400	15.5	.06	23	1.8	12	.12	24	2.1	2.4/1.4	3.5/5.6
1410	15.5	.06	23	1.8	12	.1	24	2.1	2.4/1.00	3.4/5.7
1420	13.5	.07	24	1.4	12	.1	24	2	2.8/.9	3.2/5.8
1430	11.2	.1	23	1.8	11.5	.1	23	1.8	2.7/1.8	3.8/5.6
1440	13.5	.07	23	1.9	12	.1	24	2	2.7/1.5	3.6/5.6
1450	14	.06	23	1.9	12.5	.09	24	2	2.7/1.9	3.5/5.5
1500 1500	14.5	.06	23	1.7	12.5	.1	24	2	2.6/1.3	3.6/5.5
1510	14.5	.06	23	1.7	12	.1	24.5	1.8	2.6/1.2	3.6/5.5
1520	15	.06	23	1.8	12	.1	24	1.8	2.5/1.2	3.4/5.8
1530	15.5	.05	22	2.1	12	.1	24	2	2.8/1.8	3.6/5.8
1540	16	.04	22	2.2	12.5	.09	24	2	2.8/.9	3.8/5.5
1550	15	.05	23	1.8	12.5	.1	24	2	2.6/1.4	3.7/5.8
1600	15	.06	23	1.7	12	.09	22	1.3	2.5/1.6	3.6/5.8
1610	15	.06	24	1.6	12	.09	22	1.3	2.5/1	3.8/5.8
1620	15	.05	23	1.7	12.5	.09	22	1.2	2.5/1.09	3.6/5.5
1630	15	.06	23	1.6	12.2	.09	22	1.2	2.5/1.9	3.7/6.1
1640	15	.06	23	1.6	12.2	.08	22	1.2	2.6/1.1	3.8/5.9
1650	15	.06	22	2	12.2	.09	22	1.2	3/1.2	3-8/5.9
1700	15	.05	23	1.8	12.5	.1	24.5	1.9	2.6/1.9	3.8/5.9
1710	15.5	.06	23	1.8	12.5	.09	24	1.9	2.6/1.1	3.9/5.9
1720	15.5	.06	24	1.8	13	.1	25	2	2.6/1.8	4/6
1730	15.5	.06	26	1.8	12.5	.09	24.5	2	2.6/1	4/5.8
1740	15.5	.05	24	1.7	12	.1	24	2	2.6/1	4/5.9
1750	15.3	.04	21	2	11	.09	23	1.6	2.9/1	4/6

EFB READINGS

DATE 6-8-94

BY J.C

PLANT: Hayward
source: _____

383
readings every 10 minutes

TIME	"A" SIDE				"B" SIDE				EFB PRESS.	BAG H. PRESS.
	BED VOLT	BED CURR.	ION VOLT	ION CURR.	BED VOLT	BED CURR.	ION VOLT	ION CURR.		
1800	16	.05	22	2.2	12	.1	24	2	2.7/1.7	4/6
1810	16	.04	23	1.9	11.5	.1	24	2	2.6/1.4	4/6
1820	15.5	.05	23	1.9	12	.1	24	2.1	2.6/1.8	4/6
1830	15.5	.05	23	1.7	11.5	.1	24	2.2	2.5/1.4	4/6
1840	15	.04	23	1.6	11.5	.12	24	2.2	2.2/1.8	4/6
1850	16	.06	22	2.2	12	.14	24	2.2	2.6/1.6	4/6
1900 1855	15.5	.06	23	2	11.5	.12	24	2.2	2.6/1.4	4/6
1910	16	.06	23	1.9	11.5	.12	24	2.1	2.5/1.9	4/6
1920	14.5	.06	23	1.7	11.5	.11	24	2.1	2.5/1.4	4/6.1
1930	15	.06	23	1.7	11.5	.11	24	2.1	2.5/1.9	4/6
1940	14.5	.06	22	2	11.5	.1	24	2.1	2.7/1.4	3.9/6
1950										
2000										
2010										
2020										
2030										
2040										
2050										
2100										
2110										
2120										
2130										
2140										
2150										
2200										
2210										
2220										
2230										
2240										
2250										

EFB READINGS

DATE 6-9-94
BY 103

PLANT: Hayward
SOURCE: _____

readings every 10 minutes

TIME	*A* SIDE <u>K1 & K2</u>				*B* SIDE <u>K3 & K4</u>				EFB PRESS.	BAG H. PRESS.
	BED VOLT	BED CURR.	ION VOLT	ION CURR.	BED VOLT	BED CURR.	ION VOLT	ION CURR.		
0840	14	.09	24	1.8					2.3	3.4 3.5
0850	14.5	.09	24	1.8					2.3	3.4 3.5
0900	15	.08	24	1.8					2.3	3.4 3.5
0910	14.5	.09	24.5	1.8					2.3	3.5
0920	15	.09	24	1.8					2.4	3.5
0930	15	.08	24	1.8					2.4	4
0940	15	.08	24	1.8					2.4	3.6
0950	15	.08	24	1.8					2.3	3.4
1000	15	.08	24	1.8					2.3	3.5
1010	14.5	.09	24	1.8					2.4	3.6
1020	14.5	.09	24	1.7					2.4	3.9
1030	15	.09	24	1.8					2.4	3.8
1040	14.5	.09	24	1.8					2.4	3.6
1050	15	.08	24	1.9					2.4	3.7
1100	14.5	.09	24	1.8					2.4	3.7
1110	14.5	.09	24	1.8					2.4	3.6
1120	14.7	.09	24	1.8					2.4	3.7
1130	15	.08	24	1.8					2.4	3.8
1140	15	.08	24	1.9					2.4	3.6
1150	15	.08	24	1.9					2.4	3.8
1200	15	.08	24	1.8					2.3	3.8
1210	15.0	.09	25	1.8					2.4	3.9
1220	14.5	.09	24.5	1.8					2.3	4
1230	15	.08	24	1.8					2.4	3.9
1240	14.5	.08	24	1.8					2.3	4
1250	14.5	.08	24	1.8					2.3	4

EFB READINGS

DATE 6/9/94

BY 2073

PLANT: Hayward

source:

readings every 10 minutes

TIME	"A" SIDE				"B" SIDE				EFB PRESS.	BAG H. PRESS.
	BED VOLT	BED CURR.	ION VOLT	ION CURR.	BED VOLT	BED CURR.	ION VOLT	ION CURR.		
1300	14	.1	24	1.8					2.3	3.8
1310	14.5	.1	24.5	1.8					2.3	4
1320	14.5	.09	24	1.8					2.4	4.1
1330	13.5	.1	24	1.7					2.3	4
1340	13.5	.1	24	1.7					2.3	4
1350	14	.1	24	1.8					2.3	4
1400	13.5	.1	24	1.8					2.3	3.5
1410	13	.1	24	1.8					2.3	4
1420	13.5	.1	24	1.8					2.3	4
1430	13.5	.1	24	1.8					2.3	4.1
1440	13.5	.1	24	1.8					2	4.2
1450	14	.09	24	2.2					2.3	4.1
1500	14.5	.09	24	2					2.4	4.1
1510	15	.09	24	2					2.3	4.1
1520	14	.1	24	2					2.3	3.9
1530	14.5	.1	24	2					2.3	4
1540	14.5	.1	24	1.8					2.3	4.3
1550	14	.1	24	1.9					2.3	4
1600	14	.1	24	1.8					2.3	4.1
1610	13.5	.1	24	1.8					2.3	4
1620	13.5	.08	24	1.8					2.3	4.1
1630	14	.1	24	2					2.3	4.1
1640	14	.1	24	2					2.3	4.1
1650	13.7	.1	24	1.8					2.2	4
1700	13.5	.1	24	1.9					2.3	4.2
1710	13.5	.1	24	1.8					2.3	4
1720	13	.11	24	1.8					2.3	4.1
1730	13.5	.12	24	1.9					2.3	4.2
1740	14	.12	24	1.8					2.3	4.2
1750	12.5	.14	24	1.8					2.4	4.2

EFB READINGS

DATE 6/9/94
BY 363

PLANT: Hayward
SOURCE: 1

readings every 10 minutes

TIME	"A" SIDE				"B" SIDE				EFB PRESS.	BAG H. PRESS.
	BED VOLT	BED CURR.	ION VOLT	ION CURR.	BED VOLT	BED CURR.	ION VOLT	ION CURR.		
1800	12.5	.14	24	1.9					2.4	4.2
1810	12.5	.15	24.5	1.8					2.4	4.2
1820	12.2	.15	24	1.8					2.4	4.2
1830	12.2	.15	24	1.7					2.4	4.2
1840	12	.15	24	1.8					2.4	4.2
1850	12.5	.14	24	1.8					2.4	4.2
1900	12	.15	24	1.8					2.4	4.2
1910										
1920										
1930										
1940										
1950										
2000										
2010										
2020										
2030										
2040										
2050										
2100										
2110										
2120										
2130										
2140										
2150										
2200										
2210										
2220										
2230										
2240										
2250										

6-7-94 1D

Konus-bark moisture content

8:00am - 37.9

9:00 - 38.8

10:00 - 37.9

11:00 - 40.6

12:00 - 40.8

1:00 - 42.6

2:00 - 39.5

3:00 - 36.5

4:00 - 38.8

5:00 - 37.1

6-8-94 1D

Konus - bark moisture

8:00am 39.7

9:00 40.6

10:00 39.1

11:00 39.4

12:00 40.4

1:00 38.5

2:00 38.5

3:00 34.5

4:00 38.5

5:00 40.6

6:00 40.5

7:00 39.2 2-B

8:00

9:00

10:00

11:00

6-9-94
BARK MOISTURE % (RONUS)

8:00 A.M. - 40.7%

9 - 37.4%

10 - 35.7%

11 - 37.7%

PM 12 - 36.1%

1 - 36.0%

2 - 37.7%

3 - 38.0%

4 - 37.6%

5 - 37.4%

6 - 39.6%

7 - 38.4%

Hayward
6-7-94
Turn % 1/16

.....
2,312.00 +
.....
2,312.00 *
.....
2,312.00 ÷

194.00 +
190.00 +
194.00 +
192.00 +
190.00 +
192.00 +
194.00 +
190.00 +
192.00 +
194.00 +
196.00 +
.....

LII Before - 2313
After - 2131

194 192
190 190 7.9%
194 192
192 194
190 194
194 196

.....
2,224.000 +
.....
187.000 +
190.000 +
184.000 +
187.000 +
181.000 +
186.000 +
179.000 +
189.000 +
184.000 +
186.000 +
186.000 +
185.000 +
.....

LI Before - 2,224
After - 2,086

187 179
190 189 6.2%
184 184
187 186
181 185
186 186

APPENDIX K

PROCEDURES

Particulate Loading and Emission Rates

The particulate emission rates were determined per EPA Methods 1 - 5, CFR Title 40, Part 60, Appendix A (revised July 1, 1992). In this procedure a preliminary velocity profile of the gases in the flue is obtained by means of a temperature and velocity traverse. On the basis of these values, sampling nozzles of appropriate diameter are selected to allow isokinetic sampling, a necessary prerequisite for obtaining a representative sample.

The sampling train consists of a heated glass-lined sampling probe equipped with a Type S pitot and a thermocouple. The probe is attached to a sampling module which houses the all-glass in line filter holder in a temperature controlled oven. The sampling module also houses the impinger case and a Drierite filled column. The sampling module is connected by means of an umbilical cord to the control module. The control module houses the dry test gas meter, the calibrated orifice, a leakless pump, two inclined manometers, and all controls required for operating the sampling train.

Particulate samples are collected as follows: The sample gas is drawn through the sampling probe isokinetically and passed through a 4-inch diameter Gelman Type A/E glass fiber filter where particulates are removed. The sample gas is then passed through an ice-cooled impinger train and a desiccant-packed column which absorbs remaining moisture. The sample gas then passes through a vacuum pump followed by a dry test gas meter. The gas meter integrates the sample gas flow throughout the course of the test. A calibrated orifice attached to the outlet of the gasmeter provides real time flow rate data.

A representative particulate sample was acquired by sampling for equal periods of time at the centroid of a number of equal area regions in the duct. The sampling rate is adjusted at each test point maintaining isokinetic sampling conditions. Nomographs are used for rapid determination of the sampling rate.

Particulate Loading and Emission Rates

After sampling is complete, the filter is removed and placed in a clean container. The nozzle and inlet side of the filter holder are quantitatively washed with acetone and the washings are stored in a second container. A brush is often used in the cleaning step to help dislodge deposits. The samples are returned to the laboratory where they are logged in and analyzed. The volume of the acetone rinse ("probe wash") is noted and then the rinse is quantitatively transferred to a tared 120 cc porcelain evaporating dish and the acetone evaporated off at 97-105 °F. This temperature is used to prevent condensation of atmospheric moisture due to the cooling effect induced by the evaporation of acetone. The acetone-free sample is then transferred to an oven and dried at 105 °C for 30 minutes, cooled in a desiccator over Drierite, and then weighed to the nearest .01 mg. The filter sample is quantitatively transferred to a 6-inch watch glass and dried in an oven at 105 °C for two hours. The filter and watch glass are then cooled in a desiccator and the filter weighed to the nearest .01 mg. All weighings are performed in a balance room where the relative humidity is hydrostatted to less than 50% relative humidity. Microscopic examination of the samples is performed if any unusual characteristics are observed. The weight of the acetone rinse is corrected for the acetone blank. The Drierite column is weighed on-site and the water collected by Drierite is added to the condensate so that the total amount of absorbed water may be ascertained.

Integrated flue gas samples for Orsat analysis were collected simultaneously with each pollutant sample. The samples were collected in 15-liter gas sampling bags at a constant flow rate throughout each particulate run. The bags were at a constant flow rate throughout each particulate run. The bags were then returned to the laboratory and analyzed by Orsat analysis. Standard commercially prepared solutions were used in the Orsat analyzer (sat. KOH for carbon dioxide and reduced methylene blue for oxygen).

Condensible Organic Compounds Analysis

Method II-8672

Equipment: Separatory funnel - 500 cc with Teflon stopcock

 Powder funnel - 75 mm ID with a 17 mm stem

 Evaporating dish (es) - 200 cc or 250 cc beaker

Reagents: Diethyl ether - reagent grade

 Chloroform - reagent grade

 Sodium sulfate - (ACS) granular anhydrous

 Toluene - (if 3% hydrogen peroxide is used to collect the samples)

 Glass wool (Pyrex microfiber)

PREPARATION

1. Place 1 kg of granular anhydrous sodium sulfate in a shallow tray and heat to 200°C for at least four hours. Store in a tightly sealed glass container.
2. Place a plug of clean glass wool in the stem of the powder funnel. The plug must be of sufficient size so that it is held snugly in place by its own pressure. Add a one-inch layer of dry sodium sulfate.

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SAMPLING

An all-glass impinger assembly is used in the back half of the EPA Method 5 sampling train when an organic wet catch is to be collected. The impinger assembly consists of a modified impinger, a Greenburg Smith impinger followed by another modified impinger. The third impinger should have a temperature measuring device at the outlet upstream of a final impinger or desiccant column to monitor the temperature of the outlet gas stream. Prior to the start of the test, each of the first two impingers should be charged with 100 g of Class I water. The method 5 train should be operated as provided for in EPA method 5. Ice should be added to the impinger batch to keep the temperature of the gas at the outlet at or less than 68°F. After the post test leak check, the impinger train is removed and impinger contents poured into a tared all-glass sample bottle and closed with a Teflon-lined cap. The sample bottle is then weighed and the total condensate calculated by subtraction of the bottle tare weight and the weight of initial water added to the impingers (200 g). A label is affixed and the sample is returned to the laboratory for analysis. The sample should be stored at 4°C if the analysis is not conducted within 48 hours.

I. ORGANICS

Caution! Work in vented hood!!!

A. Organic Blank Determination

1. Pour 125 ml of ethyl ether and 125 ml of chloroform into a tared beaker.
2. Evaporate solvent in hood at 70°F or less until no solvent remains.
3. Desiccate the sample in dish for two hours.
4. Weigh the sample to nearest 0.1 mg, record and report on Form LSC-03G.

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B. Organic Sample Determination

1. Test for peroxide in sample ether using KI strips. (If KI strip shows positive, contact your supervisor before proceeding.)
2. Transfer the sample solution quantitatively to a 500 ml separatory funnel. Use the first of three 25 ml chloroform aliquots to rinse the sample container.
3. Extract with three 25 ml portions of chloroform. (Shake and vent to release pressure about 4 to 5 times each.) Allow the phases to separate. (Bottom layer is chloroform.) Draw off the bottom layer, transferring the solvent with a funnel containing a plug of sodium sulfate into a tared beaker. (Do not draw off any of the aqueous layer.)
4. After the three chloroform extractions, use two 25 ml portions of chloroform to rinse the sodium sulfate, collecting the rinses in the same tared beaker as the extracts.
5. Next extract the sample three times with 25 ml aliquots of ethyl ether. (Shake and vent to release pressure about 4 to 5 times each.) Allow the phases to separate. (Top layer is ethyl ether.) Draw off the bottom layer (aqueous) into another separatory funnel taking less than 1 ml of the ethyl ether layer with. Decant the ethyl ether, passing it through sodium sulfate and collecting the ethyl ether in the same tared dish as the chloroform.
6. After the three ethyl ether extractions, take two 25 ml portions of ethyl ether and rinse the sodium sulfate collecting the rinses in the same tared beaker as the extracts.
7. Evaporate the solvents (chloroform and ethyl ether) in the tared beaker in the hood at 70°F or less until no solvent remains. (Use no heat and have no sources of ignition in the hood when doing this procedure.) Do not evaporate so quickly as to allow evaporative cooling to lower the temperature of the container below the dew point of water, otherwise, water will be condensed out in the container.

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8. Desiccate to constant weight (two hours). Record and report the final weight to the nearest 0.1 mg on Form LSC-03G.

II. INORGANICS

If inorganic residue information is required, the following procedure should be conducted:

A. Inorganic Blank Determination

1. Vent the remaining aqueous phase from the organic extraction in the hood to remove residual organic solvents (usually overnight).
2. Decant the impinger catch into a tared evaporating dish.
3. Evaporate all of the water in the sample in an oven at 100°C. Take care not to boil to prevent bumping and loss of sample.
4. Cool the dried sample in the desiccator and desiccate until a constant weight is obtained.
5. Report the results to the nearest 0.1 mg on Form LSC-03G.

B. Inorganic Sample Determination

Follow steps 1-5 in Section A above.

NOTES

1. For the organics determination, in the rare event that the impinger catch resulted from a Modified Method 6 determination (SO_2), whereby the solution contains dilute hydrogen peroxide ($\geq 3\%$), do not use ether as an extraction solvent. Substitute toluene for ethyl ether in Section I. (Ether in the presence of peroxide forms explosive hydroperoxide.)

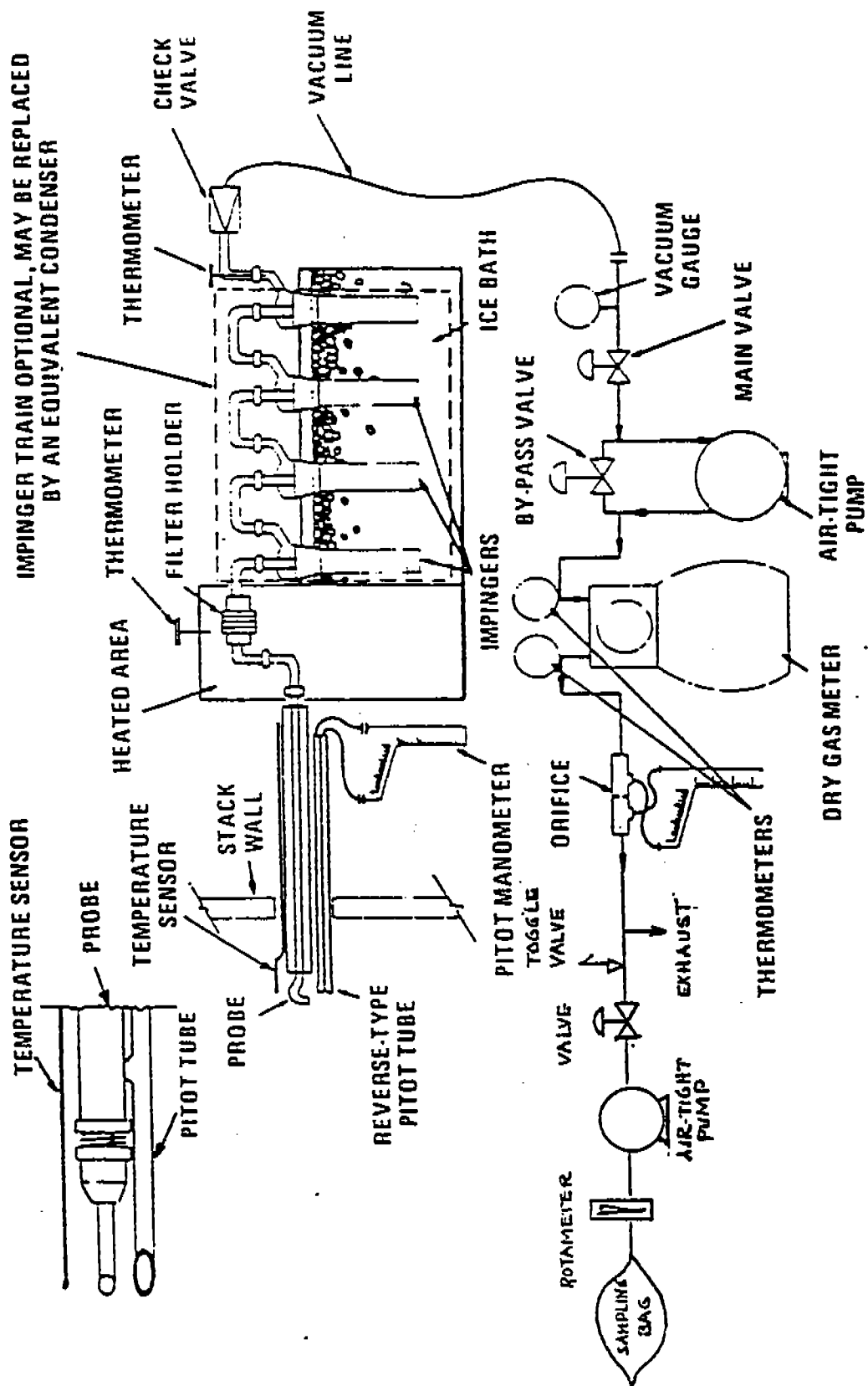
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2. In the organics determination, more than three extractions may be required to extract all of the organics. Additional extractions should be performed if the aqueous phase is still cloudy.
3. Special state requirements:
 - Michigan - Total sample evaporated in tared evaporating dish on steam bath.
 - Iowa - Organics and inorganics separately, as required.
 - Wisconsin - Use Method II-8672-WI.
 - Rest of states - Organics only.

REFERENCES

Proposed standards of Performance for New Stationary Sources, Federal Register 36(159) Part II, August 1, 1979.

Minnesota Pollution Control Agency, Exhibit C.



Particulate-sampling train.

Flow

Flow determinations were carried out in accordance with EPA Method 2, CFR Title 40, Part 60, Appendix A (Revised July 1, 1987). A type S pitot was used to sense velocity pressure and an inclined manometer was used to measure velocity pressures. Gas temperatures were measured using a calibrated Type K thermocouple and digital temperature meter. Gas density (i.e. molecular weight) was calculated from the composition of the gas which was determined by Orsat.

Gas Flow Density

Gas compositions were determined as per Method 3 by Orsat analysis of an integrated gas sample collected from the stack during the oxides of nitrogen determinations. Standard commercially prepared solutions were used in the Orsat analyzer (sat. KOH for carbon dioxide and reduced methylene blue for oxygen).

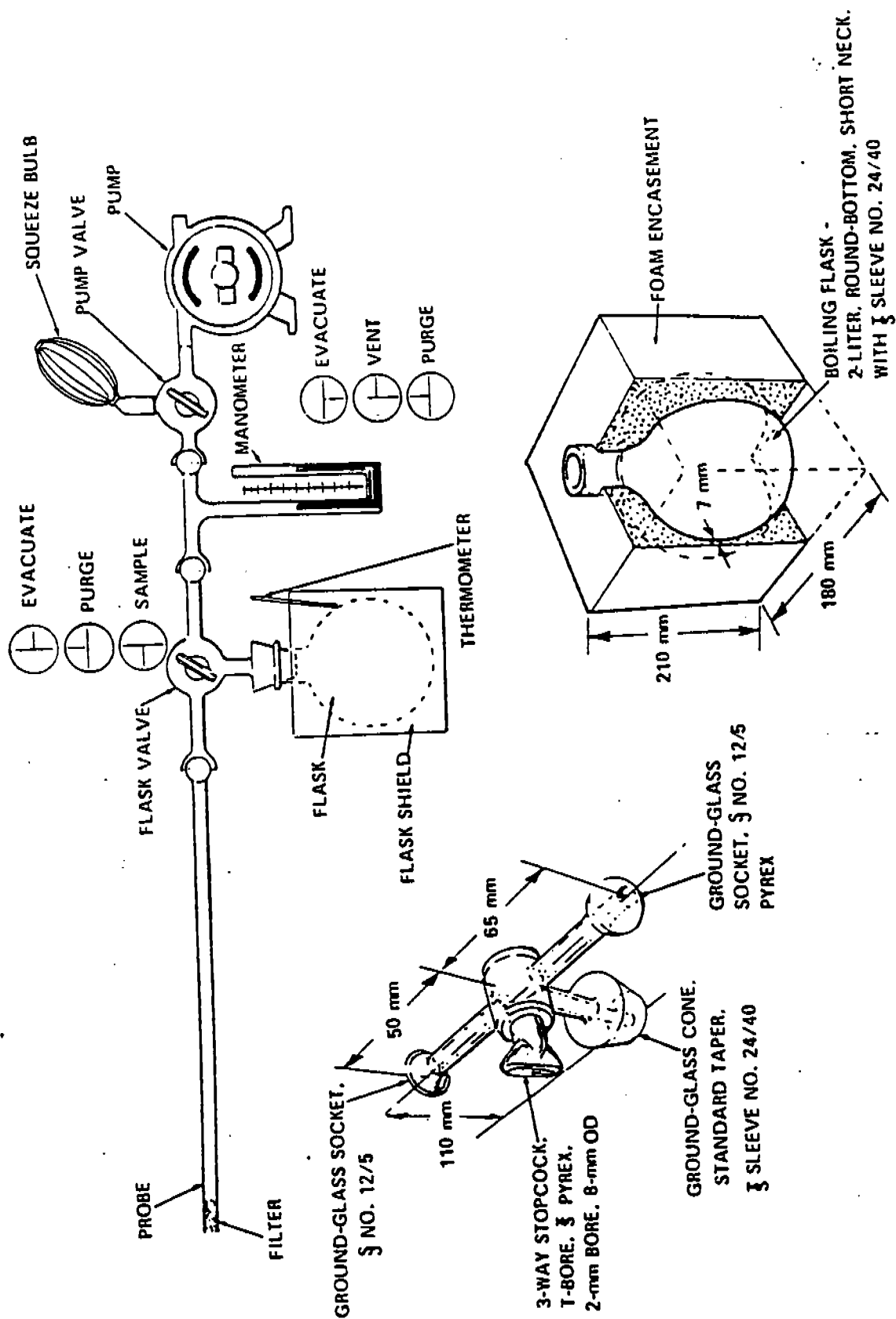
Oxides of Nitrogen

Oxides of nitrogen concentrations were collected in accordance with EPA Method 7 (see above-cited reference) with a specially designed all glass manifold and valving assembly and a heated stainless steel-lined probe. Samples were collected in two-liter evacuated insulated flasks which contained 25 cc of acidified peroxide solution (Method 7 reagent). Nine sets or more of three samples each were collected over a period of 4.5 to 5 hours.

The sampling train was leak checked through the probe at the beginning and end of the test and, in addition, the system leak checked at the time of evacuation of each flask. Before the samples were collected, the probe was purged to eliminate dead volume effects and to raise the temperature of the probe outlet and manifold assembly to minimize condensation of moisture. A plug of microfiber glass wool inserted in the probe inlet was used to prevent particulate material from entering into the flask. The temperature of the flask, vacuum in the

flask and barometric pressure at the time of sampling was recorded for each flask. After sampling was complete, as evidenced by the in-line vacuum gauge, the flask valve was closed, the flask assembly disconnected from the manifold/valve assembly and the flask shook for several minutes to promote oxidation and absorption. The recovered oxides of nitrogen samples were returned to the laboratory and analyzed immediately by ion chromatography as per EPA 7A.

The internal volume of each numbered flask assembly has been measured prior to initial use by filling with water, weighing before and after and then converting the weight of water to volume by means of the density of water at room temperature. Flask volumes are stored in the computer and recalled automatically in the computer calculation.



Sampling train, flask valve, and flask.

4.2 Performance Evaluation Tests. The owner of a lidar system shall subject such a lidar system to the performance verification tests described in Section 3, prior to first use of this method. The annual calibration shall be performed for three separate, complete runs and the results of each should be recorded. The requirements of Section 3.3.1 must be fulfilled for each of the three runs.

Once the conditions of the annual calibration are fulfilled the lidar shall be subjected to the routine verification for three separate complete runs. The requirements of Section 3.3.2 must be fulfilled for each of the three runs and the results should be recorded. The Administrator may request that the results of the performance evaluation be submitted for review.

5. References

5.1 The Use of Lidar for Emissions Source Opacity Determination, U.S. Environmental Protection Agency, National Enforcement Investigations Center, Denver, CO. EPA-330/1-79-003-R, Arthur W. Dybdahl, current edition [NTIS No. PB81-246662].

5.2 Field Evaluation of Mobile Lidar for the Measurement of Smoke Plume Opacity, U.S. Environmental Protection Agency, National Enforcement Investigations Center, Denver, CO. EPA/NEIC-TS-128, February 1976.

5.3 Remote Measurement of Smoke Plume Transmittance Using Lidar, C. S. Cook, G. W. Bethke, W. D. Conner (EPA/RTP). Applied Optics 11, pg 1742. August 1972.

5.4 Lidar Studies of Stack Plumes in Rural and Urban Environments, EPA-650/4-73-002, October 1973.

5.5 American National Standard for the Safe Use of Lasers ANSI Z 136.1-176, March 8, 1976.

5.6 U.S. Army Technical Manual TB MED 279, Control of Hazards to Health from Laser Radiation, February 1969.

5.7 Laser Institute of America Laser Safety Manual, 4th Edition.

5.8 U.S. Department of Health, Education and Welfare, Regulations for the Administration and Enforcement of the Radiation Control for Health and Safety Act of 1968, January 1976.

5.9 Laser Safety Handbook, Alex Mallow, Leon Chabot, Van Nostrand Reinhold Co., 1978.

METHOD 10—DETERMINATION OF CARBON MONOXIDE EMISSIONS FROM STATIONARY SOURCES

1. Principle and Applicability

1.1 Principle. An integrated or continuous gas sample is extracted from a sampling point and analyzed for carbon monoxide

(CO) content using a Luft-type nondispersive infrared analyzer (NDIR) or equivalent.

1.2 Applicability. This method is applicable for the determination of carbon monoxide emissions from stationary sources only when specified by the test procedures for determining compliance with new source performance standards. The test procedure will indicate whether a continuous or an integrated sample is to be used.

2. Range and Sensitivity

2.1 Range. 0 to 1,000 ppm.

2.2 Sensitivity. Minimum detectable concentration is 20 ppm for a 0 to 1,000 ppm span.

3. Interferences

Any substance having a strong absorption of infrared energy will interfere to some extent. For example, discrimination ratios for water (H₂O) and carbon dioxide (CO₂) are 3.5 percent H₂O per 7 ppm CO and 10 percent CO₂ per 10 ppm CO, respectively, for devices measuring in the 1,500 to 3,000 ppm range. For devices measuring in the 0 to 100 ppm range, interference ratios can be as high as 3.5 percent H₂O per 25 ppm CO and 10 percent CO₂ per 50 ppm CO. The use of silica gel and ascarite traps will alleviate the major interference problems. The measured gas volume must be corrected if these traps are used.

4. Precision and Accuracy

4.1 Precision. The precision of most NDIR analyzers is approximately ± 2 percent of span.

4.2 Accuracy. The accuracy of most NDIR analyzers is approximately ± 5 percent of span after calibration.

5. Apparatus

5.1 Continuous Sample (Figure 10-1).

5.1.1 Probe. Stainless steel or sheathed Pyrex¹ glass, equipped with a filter to remove particulate matter.

5.1.2 Air-Cooled Condenser or Equivalent. To remove any excess moisture.

5.2 Integrated Sample (Figure 10-2).

5.2.1 Probe. Stainless steel or sheathed Pyrex glass, equipped with a filter to remove particulate matter.

5.2.2 Air-Cooled Condenser or Equivalent. To remove any excess moisture.

5.2.3 Valve. Needle valve, or equivalent, to adjust flow rate.

5.2.4 Pump. Leak-free diaphragm type, or equivalent, to transport gas.

5.2.5 Rate Meter. Rotameter, or equivalent, to measure a flow range from 0 to 1.0 liter per min (0.035 cfm).

¹ Mention of trade names or specific products does not constitute endorsement by the Environmental Protection Agency.

5.2.6 Flexible Bag. Tedlar, or equivalent, with a capacity of 60 to 90 liters (2 to 3 ft³). Leak-test the bag in the laboratory before using by evacuating bag with a pump followed by a dry gas meter. When evacuation is complete, there should be no flow through the meter.

5.2.7 Pitot Tube. Type S, or equivalent, attached to the probe so that the sampling rate can be regulated proportional to the stack gas velocity when velocity is varying with the time or a sample traverse is conducted.

5.3 Analysis (Figure 10-3).

5.3.1 Carbon Monoxide Analyzer. Nondispersive infrared spectrometer, or equivalent. This instrument should be demonstrated, preferably by the manufacturer, to meet or exceed manufacturer's specifications and those described in this method.

5.3.2 Drying Tube. To contain approximately 200 g of silica gel.

5.3.3 Calibration Gas. Refer to section 6.1.

5.3.4 Filter. As recommended by NDIR manufacturer.

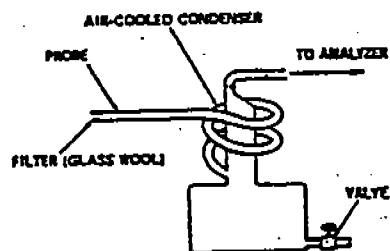


Figure 10-1. Continuous sampling train.

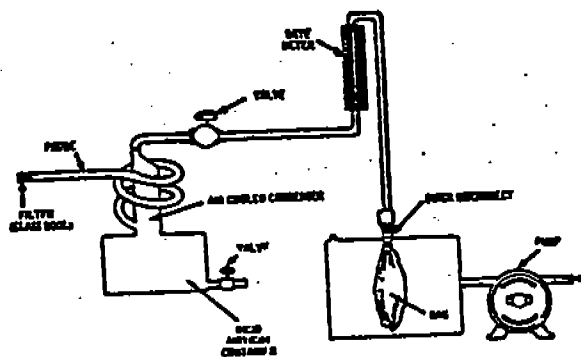


Figure 10-2. Integrated gas sampling train.

5.3.5 CO₂ Removal Tube. To contain approximately 500 g of ascarite.

5.3.6 Ice Water Bath. For ascarite and silica gel tubes.

5.3.7 Valve. Needle valve, or equivalent, to adjust flow rate

5.3.8 Rate Meter. Rotameter or equivalent to measure gas flow rate of 0 to 1.0 liter per min (0.035 cfm) through NDIR.

5.3.9 Recorder (optional). To provide permanent record of NDIR readings.

6. Reagents

6.1 Calibration Gases. Known concentration of CO in nitrogen (N₂) for instrument span, prepurified grade of N₂ for zero, and two additional concentrations corresponding approximately to 60 percent and 30 percent span. The span concentration shall not exceed 1.5 times the applicable source performance standard. The calibration gases shall be certified by the manufacturer to be within ± 2 percent of the specified concentration.

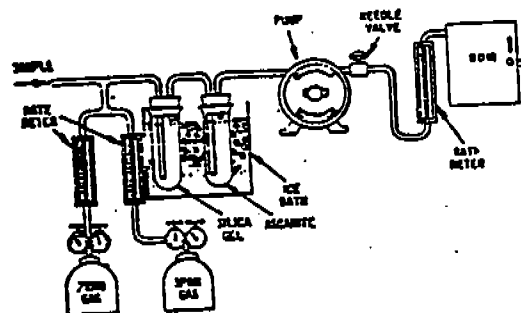


Figure 10-3. Analytical equipment.

6.2 Silica Gel. Indicating type, 6 to 16 mesh, dried at 175° C (347° F) for 2 hours.

6.3 Ascarite. Commercially available.

7. Procedure

7.1 Sampling.

7.1.1 Continuous Sampling. Set up the equipment as shown in Figure 10-1 making sure all connections are leak free. Place the probe in the stack at a sampling point and purge the sampling line. Connect the analyzer and begin drawing sample into the analyzer. Allow 5 minutes for the system to stabilize, then record the analyzer reading as required by the test procedure. (See section 7.2 and 8). CO₂ content of the gas may be determined by using the Method 3 integrated sample procedure, or by weighing the ascarite CO₂ removal tube and computing CO₂ concentration from the gas volume sampled and the weight gain of the tube.

7.1.2 Integrated Sampling. Evacuate the flexible bag. Set up the equipment as shown in Figure 10-2 with the bag disconnected. Place the probe in the stack and purge the sampling line. Connect the bag, making sure that all connections are leak free. Sample at a rate proportional to the stack velocity. CO₂ content of the gas may be determined by using the Method 3 integrated sample procedures, or by weighing the ascarite CO₂ removal tube and computing CO₂ concentra-

METHOD 25A—DETERMINATION OF TOTAL GASEOUS ORGANIC CONCENTRATION USING A FLAME IONIZATION ANALYZER

1. Applicability and Principle

1.1 Applicability. This method applies to the measurement of total gaseous organic concentration of vapors consisting primarily of alkanes, alkenes, and/or arenes (aromatic hydrocarbons). The concentration is expressed in terms of propane (or other appropriate organic calibration gas) or in terms of carbon.

1.2 Principle. A gas sample is extracted from the source through a heated sample line, if necessary, and glass fiber filter to a flame ionization analyzer (FIA). Results are reported as volume concentration equivalents of the calibration gas or as carbon equivalents.

2. Definitions

2.1 Measurement System. The total equipment required for the determination of the gas concentration. The system consists of the following major subsystems:

2.1.1 Sample Interface. That portion of the system that is used for one or more of the following: sample acquisition, sample transportation, sample conditioning, or protection of the analyzer from the effects of the stack effluent.

2.1.2 Organic Analyzer. That portion of the system that senses organic concentration and generates an output proportional to the gas concentration.

2.2 Span Value. The upper limit of a gas concentration measurement range that is

specified for affected source categories in the applicable part of the regulations. The span value is established in the applicable regulation and is usually 1.5 to 2.5 times the applicable emission limit. If no span value is provided, use a span value equivalent to 1.5 to 2.5 times the expected concentration. For convenience, the span value should correspond to 100 percent of the recorder scale.

2.3 Calibration Gas. A known concentration of a gas in an appropriate diluent gas.

2.4 Zero Drift. The difference in the measurement system response to a zero level calibration gas before and after a stated period of operation during which no unscheduled maintenance, repair, or adjustment took place.

2.5 Calibration Drift. The difference in the measurement system response to a mid-level calibration gas before and after a stated period of operation during which no unscheduled maintenance, repair or adjustment took place.

2.6 Response Time. The time interval from a step change in pollutant concentration at the inlet to the emission measurement system to the time at which 95 percent of the corresponding final value is reached as displayed on the recorder.

2.7 Calibration Error. The difference between the gas concentration indicated by the measurement system and the known concentration of the calibration gas.

3. Apparatus

A schematic of an acceptable measurement system is shown in Figure 25A-1. The essential components of the measurement system are described below:

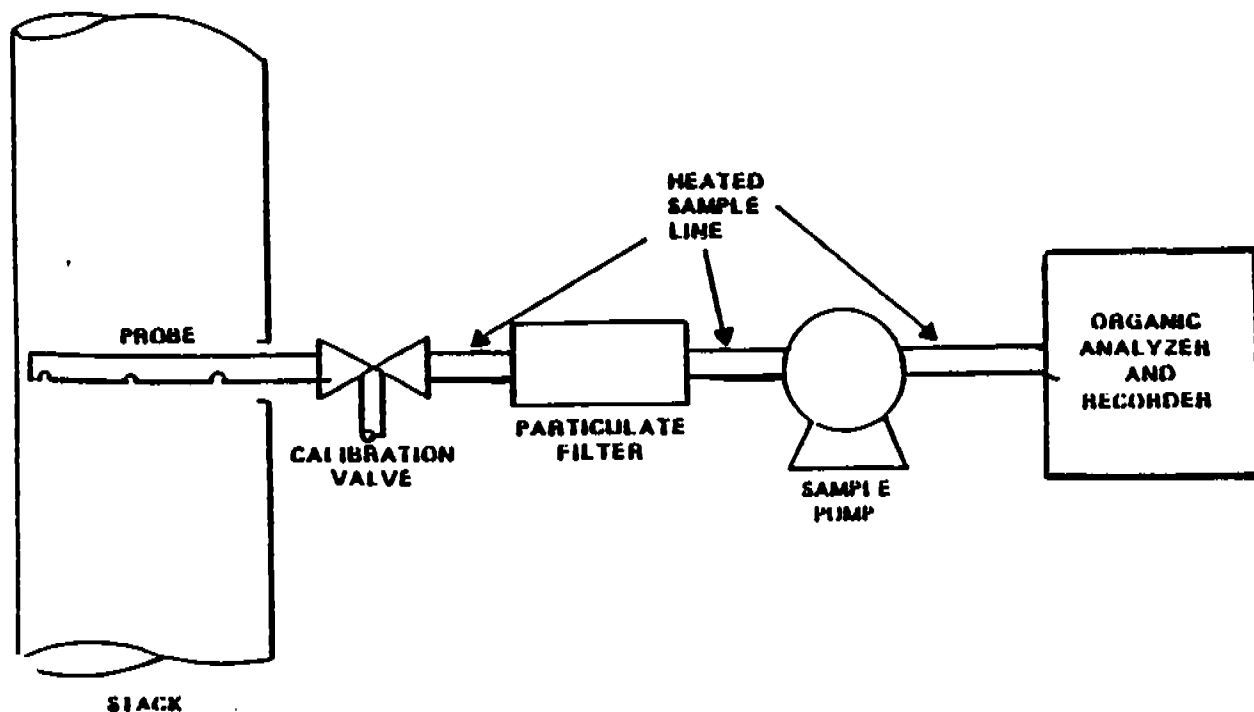


Figure 25A-1. Organic Concentration Measurement System.

3.1 Organic Concentration Analyzer. A flame ionization analyzer (FLA) capable of meeting or exceeding the specifications in this method.

3.2 Sample Probe. Stainless steel, or equivalent, three-hole rake type. Sample holes shall be 4 mm in diameter or smaller and located at 16.7, 50, and 83.3 percent of the equivalent stack diameter. Alternatively, a single opening probe may be used so that a gas sample is collected from the centrally located 10 percent area of the stack cross-section.

3.3 Sample Line. Stainless steel or Teflon* tubing to transport the sample gas to the analyzer. The sample line should be heated, if necessary, to prevent condensation in the line.

3.4 Calibration Valve Assembly. A three-way valve assembly to direct the zero and calibration gases to the analyzers is recommended. Other methods, such as quick-connect lines, to route calibration gas to the analyzers are applicable.

3.5 Particulate Filter. An in-stack or an out-of-stack glass fiber filter is recommended if exhaust gas particulate loading is significant. An out-of-stack filter should be heated to prevent any condensation.

3.6 Recorder. A strip-chart recorder, analog computer, or digital recorder for recording measurement data. The minimum data recording requirement is one measurement value per minute. Note: This method is often applied in highly explosive areas. Caution and care should be exercised in choice of equipment and installation.

4. Calibration and Other Gases

Gases used for calibrations, fuel, and combustion air (if required) are contained in compressed gas cylinders. Preparation of calibration gases shall be done according to the procedure in Protocol No. 1, listed in Reference 9.2. Additionally, the manufacturer of the cylinder should provide a recommended shelf life for each calibration gas cylinder over which the concentration does not change more than ± 2 percent from the certified value. For calibration gas values not generally available (i.e., organics between 1 and 10 percent by volume), alternative methods for preparing calibration gas mixtures, such as dilution systems, may be used with prior approval of the Administrator.

Calibration gases usually consist of propane in air or nitrogen and are determined in terms of the span value. Organic compounds other than propane can be used following the above guidelines and making the appropriate corrections for response factor.

* Mention of trade names or specific products does not constitute endorsement by the Environmental Protection Agency.

4.1 Fuel. A 40 percent H_2 /60 percent He or 40 percent H_2 /60 percent N_2 gas mixture is recommended to avoid an oxygen synergism effect that reportedly occurs when oxygen concentration varies significantly from a mean value.

4.2 Zero Gas. High purity air with less than 0.1 parts per million by volume (p.p.m.) of organic material (propane or carbon equivalent) or less than 0.1 percent of the span value, whichever is greater.

4.3 Low-level Calibration Gas. An organic calibration gas with a concentration equivalent to 25 to 35 percent of the applicable span value.

4.4 Mid-level Calibration Gas. An organic calibration gas with a concentration equivalent to 45 to 55 percent of the applicable span value.

4.5 High-level Calibration Gas. An organic calibration gas with a concentration equivalent to 80 to 90 percent of the applicable span value.

5. Measurement System Performance Specifications

5.1 Zero Drift. Less than ± 3 percent of the span value.

5.2 Calibration Drift. Less than ± 3 percent of span value.

5.3 Calibration Error. Less than ± 5 percent of the calibration gas value.

6. Pretest Preparations

6.1 Selection of Sampling Site. The location of the sampling site is generally specified by the applicable regulation or purpose of the test; i.e., exhaust stack, inlet line, etc. The sample port shall be located at least 1.5 meters or 2 equivalent diameters upstream of the gas discharge to the atmosphere.

6.2 Location of Sample Probe. Install the sample probe so that the probe is centrally located in the stack, pipe, or duct and is sealed tightly at the stack port connection.

6.3 Measurement System Preparation. Prior to the emission test, assemble the measurement system following the manufacturer's written instructions in preparing the sample interface and the organic analyzer. Make the system operable.

FLA equipment can be calibrated for almost any range of total organics concentrations. For high concentrations of organics (> 1.0 percent by volume as propane) modifications to most commonly available analyzers are necessary. One accepted method of equipment modification is to decrease the size of the sample to the analyzer through the use of a smaller diameter sample capillary. Direct and continuous measurement of organic concentration is a necessary consideration when determining any modification design.

6.4 Calibration Error Test. Immediately prior to the test series, (within 2 hours of the start of the test) introduce zero gas and

high-level calibration gas at the calibration valve assembly. Adjust the analyzer output to the appropriate levels, if necessary. Calculate the predicted response for the low-level and mid-level gases based on a linear response line between the zero and high-level responses. Then introduce low-level and mid-level calibration gases successively to the measurement system. Record the analyzer responses for low-level and mid-level calibration gases and determine the differences between the measurement system responses and the predicted responses. These differences must be less than 5 percent of the respective calibration gas value. If not, the measurement system is not acceptable and must be replaced or repaired prior to testing. No adjustments to the measurement system shall be conducted after the calibration and before the drift check (Section 7.3). If adjustments are necessary before the completion of the test series, perform the drift checks prior to the required adjustments and repeat the calibration following the adjustments. If multiple electronic ranges are to be used, each additional range must be checked with a mid-level calibration gas to verify the multiplication factor.

6.5 Response Time Test. Introduce zero gas into the measurement system at the calibration valve assembly. When the system output has stabilized, switch quickly to the high-level calibration gas. Record the time from the concentration change to the measurement system response equivalent to 95 percent of the step change. Repeat the test three times and average the results.

7. Emission Measurement Test Procedure

7.1 Organic Measurement. Begin sampling at the start of the test period, recording time and any required process information as appropriate. In particular, note on the recording chart periods of process interruption or cyclic operation.

7.2 Drift Determination. Immediately following the completion of the test period and hourly during the test period, reintroduce the zero and mid-level calibration gases, one at a time, to the measurement system at the calibration valve assembly. (Make no adjustments to the measurement system until after both the zero and calibration drift checks are made.) Record the analyzer response. If the drift values exceed the specified limits, invalidate the test results preceding the check and repeat the test following corrections to the measurement system. Alternatively, recalibrate the test measurement system as in Section 6.4 and report the results using both sets of calibration data (i.e., data determined prior to the test period and data determined following the test period).

8. Organic Concentration Calculations

Determine the average organic concentration in terms of ppmv as propane or other

mined by the integration of the output recording over the period specified in the applicable regulation.

If results are required in terms of ppmv as carbon, adjust measured concentrations using Equation 25A-1.

$$C_c = K C_{meas}$$

Eq. 25A-1

Where:

C_c = Organic concentration as carbon, ppmv.

C_{meas} = Organic concentration as measured, ppmv.

K = Carbon equivalent correction factor,

$K=2$ for ethane.

$K=3$ for propane.

$K=4$ for butane.

K = Appropriate response factor for other organic calibration gases.

9. Bibliography

9.1 Measurement of Volatile Organic Compounds—Guideline Series. U.S. Environmental Protection Agency. Research Triangle Park, NC. Publication No. EPA-450/2-78-041. June 1978. p. 46-54.

9.2 Traceability Protocol for Establishing True Concentrations of Gases Used for Calibration and Audits of Continuous Source Emission Monitors (Protocol No. 1). U.S. Environmental Protection Agency, Environmental Monitoring and Support Laboratory. Research Triangle Park, NC. June 1978.

9.3 Gasoline Vapor Emission Laboratory Evaluation—Part 2. U.S. Environmental Protection Agency, Office of Air Quality Planning and Standards. Research Triangle Park, NC. EMB Report No. 75-GAS-6. August 1975.

SAMPLING FOR FORMALDEHYDE EMISSIONS FROM STATIONARY SOURCES JUL 16 1990

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1.0 SCOPE AND APPLICATION

1.1 This method is applicable to the determination of Destruction and Removal Efficiency (DRE) of formaldehyde, CAS Registry number 50-00-0, and possibly other aldehydes and ketones from stationary sources as specified in the regulations. The methodology has been applied specifically to formaldehyde; however, many laboratories have extended the application to other aldehydes and ketones. Compounds derivatized with 2,4-dinitrophenylhydrazine can be detected as low as 6.4×10^{-6} lbs/cu ft (1.8 ppbv) in stack gas over a 1 h sampling period, sampling approximately 45 cu ft.

2.0 SUMMARY OF METHOD

2.1 Gaseous and particulate pollutants are withdrawn isokinetically from an emission source and are collected in aqueous acidic 2,4-dinitrophenylhydrazine. Formaldehyde present in the emissions reacts with the 2,4-dinitrophenylhydrazine to form the formaldehyde dinitrophenylhydrazone derivative. The dinitrophenylhydrazone derivative is extracted, solvent-exchanged, concentrated, and then analyzed by high performance liquid chromatography.

3.0 INTERFERENCES

3.1 A decomposition product of 2,4-dinitrophenylhydrazine, 2,4-dinitroaniline, can be an analytical interferent if concentrations are high. 2,4-dinitroaniline can coelute with the 2,4-dinitrophenylhydrazone of formaldehyde under high performance liquid chromatography conditions which may be used for the analysis. High concentrations of highly oxygenated compounds, especially acetone, that have the same retention time or nearly the same retention time as the dinitrophenylhydrazone of formaldehyde and that also absorb at 360 nm will interfere with the analysis.

Formaldehyde, acetone, and 2,4-dinitroaniline contamination of the aqueous acidic 2,4-dinitrophenylhydrazine (DNPH) reagent is frequently encountered. The reagent must be prepared within five days of use in the field and must be stored in an uncontaminated environment both before and after sampling in order to minimize blank problems. Some level of acetone contamination is unavoidable, because acetone is ubiquitous in laboratory and field operations. However, the acetone contamination must be minimized.

4.0 APPARATUS AND MATERIALS

4.1 A schematic of the sampling train is shown in Figure 1. This sampling train configuration is adapted from EPA Method 5 procedures. The sampling train consists of the following components: Probe Nozzle, Pitot Tube, Differential Pressure Gauge, Metering System, Barometer, and Gas Density Determination Equipment.

4.1.1 Probe Nozzle: Quartz or glass with sharp, tapered (30° angle) leading edge. The taper shall be on the outside to preserve a constant inner diameter. The nozzle shall be buttonhook or elbow design. A range of nozzle sizes suitable

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for isokinetic sampling should be available in increments of 0.16 cm (1/16 in), e.g., 0.32 to 1.27 cm (1/8 to 1/2 in), or larger if higher volume sampling trains are used. Each nozzle shall be calibrated according to the procedures outlined in Section 8.1.

4.1.2 Probe Liner: Borosilicate glass or quartz shall be used for the probe liner. The tester should not allow the temperature in the probe to exceed $120 \pm 14^{\circ}\text{C}$ ($248 \pm 25^{\circ}\text{F}$).

4.1.3 Pitot Tube: The Pitot tube shall be Type S, as described in Section 2.1 of EPA Method 2, or any other appropriate device. The pitot tube shall be attached to the probe to allow constant monitoring of the stack gas velocity. The impact (high pressure) opening plane of the pitot tube shall be even with or above the nozzle entry plane (see EPA Method 2, Figure 2-6b) during sampling. The Type S pitot tube assembly shall have a known coefficient, determined as outlined in Section 4 of EPA Method 2.

4.1.4 Differential Pressure Gauge: The differential pressure gauge shall be an inclined manometer or equivalent device as described in Section 2.2 of EPA Method 2. One manometer shall be used for velocity-head readings and the other for orifice differential pressure readings.

4.1.5 Impingers: The sampling train requires a minimum of four impingers, connected as shown in Figure 1, with ground glass (or equivalent) vacuum-tight fittings. For the first, third, and fourth impingers, use the Greenburg-Smith design, modified by replacing the tip with a 1.3-cm inside diameter (1/2 in) glass tube extending to 1.3 cm (1/2 in) from the bottom of the flask. For the second impinger, use a Greenburg-Smith impinger with the standard tip. Place a thermometer capable of measuring temperature to within 1°C (2°F) at the outlet of the fourth impinger for monitoring purposes.

4.1.6 Metering System: The necessary components are a vacuum gauge, leak-free pump, thermometers capable of measuring temperature within 3°C (5.4°F), dry-gas meter capable of measuring volume to within 1%, and related equipment as shown in Figure 1. At a minimum, the pump should be capable of 4 cfm free flow, and the dry gas meter should have a recording capacity of 0-999.9 cu ft with a resolution of 0.005 cu ft. Other metering systems may be used which are capable of maintaining sampling rates within 10% of isokinetic collection and of determining sample volumes to within 2%. The metering system may be used in conjunction with a pitot tube to enable checks of isokinetic sampling rates.

4.1.7 Barometer: The barometer may be mercury, aneroid, or other barometer capable of measuring atmospheric pressure to within 2.5 mm Hg (0.1 in Hg). In many cases, the barometric reading may be obtained from a nearby National Weather Service Station, in which case the station value (which is the absolute barometric pressure) is requested and an adjustment for elevation differences between the weather station and sampling point is applied at a rate of minus 2.5 mm Hg (0.1 in Hg) per 30 m (100 ft) elevation increase (vice versa for elevation decrease).

4.1.8 Gas Density Determination Equipment: Temperature sensor and pressure gauge (as described in Sections 2.3 and 2.4 of EPA Method 2), and gas analyzer, if necessary (as described in EPA Method 3). The temperature sensor ideally should be permanently attached to the pitot tube or sampling probe in a fixed

configuration such that the tip of the sensor extends beyond the leading edge of the probe sheath and does not touch any metal. Alternatively, the sensor may be attached just prior to use in the field. Note, however, that if the temperature sensor is attached in the field, the sensor must be placed in an interference-free arrangement with respect to the Type S pitot tube openings (see EPA Method 2, Figure 2-7). As a second alternative, if a difference of no more than 1% in the average velocity measurement is to be introduced, the temperature gauge need not be attached to the probe or pitot tube.

4.2 Sample Recovery

4.2.1 Probe Liner: Probe nozzle and brushes; Teflon® bristle brushes with stainless steel wire handles are required. The probe brush shall have extensions of stainless steel, Teflon®, or inert material at least as long as the probe. The brushes shall be properly sized and shaped to brush out the probe liner, the probe nozzle, and the impingers.

4.2.2 Wash Bottles: Three wash bottles are required. Teflon® or glass wash bottles are recommended; polyethylene wash bottles should not be used because organic contaminants may be extracted by exposure to organic solvents used for sample recovery.

4.2.3 Graduated Cylinder and/or Balance: A graduated cylinder or balance is required to measure condensed water to the nearest 1 mL or 1 g. Graduated cylinders shall have divisions not >2 mL. Laboratory balances capable of weighing to ± 0.5 g are required.

4.2.4 Amber Glass Storage Containers: One-liter wide-mouth amber flint glass bottles with Teflon®-lined caps are required to store impinger water samples. The bottles must be sealed with Teflon® tape.

4.2.5 Rubber Policeman and Funnel: A rubber policeman and funnel are required to aid in the transfer of materials into and out of containers in the field.

5.0 REAGENTS

Reagent grade chemicals or better grades shall be used in all tests. Unless otherwise indicated, all reagents shall conform to the specifications of the Committee on Analytical Reagents of the American Chemical Society, where such specifications are available.

5.1 Water: HPLC-grade water is used in preparation of DNPH reagent and in all other applications in the sampling train.

5.2 Silica Gel: Silica gel shall be indicating type, 6-16 mesh. If the silica gel has been used previously, dry at 175°C (350°F) for 2 h before using. New silica gel may be used as received. Alternatively, other types of desiccants (equivalent or better) may be used.

5.3 Crushed Ice: Quantities ranging from 10-50 lb may be necessary during a sampling run, depending upon ambient temperature. Samples which have been taken must be stored and shipped cold; sufficient ice for this purpose must be allowed.

5.4 2,4-Dinitrophenylhydrazine Reagent: The 2,4-dinitrophenylhydrazine reagent must be prepared in the laboratory within five days of sampling use in the field. Preparation of DNPH can also be done in the field, with consideration of appropriate procedures required for safe handling of solvent in the field. When a container of prepared DNPH reagent is opened in the field, the contents of the opened container should be used within 48 hours. All laboratory glassware must be washed with detergent and water and rinsed with water, methanol, and methylene chloride prior to use.

NOTE: The glassware must not be rinsed with acetone or unacceptable levels of acetone contamination will be introduced. If field preparation of DNPH is performed, caution must be exercised in avoiding acetone contamination.

Reagent bottles for storage of cleaned DNPH derivatizing solution must be rinsed with acetonitrile and dried before use. Baked glassware is not essential for preparation of DNPH reagent.

NOTE: DNPH crystals or DNPH solution should be handled with plastic gloves at all times, with prompt and extensive use of running water in case of skin exposure.

5.4.1 Preparation of Aqueous Acidic DNPH: The following materials and reagents are required for preparation of the reagent.

5.4.1.1 Bottles/Caps: amber 1- or 4 L bottles with Teflon®-lined caps are required for storing cleaned DNPH solution. Additional 4-L bottles are required to collect waste organic solvents.

5.4.1.2 Large Glass Container: at least one large glass container (8 to 16 L) is required for mixing the aqueous acidic DNPH solution.

5.4.1.3 Stir Plate/Large Stir Bars/Stir Bar Retriever: a magnetic stir plate and large stir bar are required for the mixing of the aqueous acidic DNPH solution. A stir bar retriever is needed for removing the stir bar from the large container holding the DNPH solution.

5.4.1.4 Buchner Filter/Filter Flask/Filter Paper: a large filter flask (2-4 L) with a buchner filter, appropriate rubber stopper, filter paper, and connecting tubing are required for filtering the aqueous acidic DNPH solution prior to cleaning.

5.4.1.5 Separatory Funnels: at least one large separatory funnel (2 L) is required for cleaning the DNPH prior to use.

5.4.1.6 Beakers: beakers (150 mL, 250 mL, and 400 mL) are useful for holding/measuring organic liquids when cleaning the aqueous acidic DNPH solution and for weighing DNPH crystals.

5.4.1.7 Funnels: at least one large funnel is needed for pouring the aqueous acidic DNPH into the separatory funnel.

5.4.1.8 Graduated Cylinders: at least one large graduated cylinder (1 to 2 L) is required for measuring HPLC-grade water and acid when preparing the DNPH solution.

5.4.1.9 Top-Loading Balance: a one-place top loading balance is needed for weighing out the DNPH crystals used to prepare the aqueous acidic DNPH solution.

5.4.1.10 Spatulas: spatulas are needed for weighing out DNPH when preparing the aqueous DNPH solution.

5.4.1.11 HPLC-Grade Water: water (HPLC-grade) is required to mix the aqueous DNPH solution.

5.4.1.12 Hydrochloric Acid: reagent grade hydrochloric acid (approximately 12N) is required for acidifying the aqueous DNPH solution.

5.4.1.13 2,4-Dinitrophenylhydrazine: a supply of moist solid 2,4-dinitrophenylhydrazine (DNPH) is required for preparation of aqueous acidic DNPH solution. The quantity of water may vary from 10 to 30%. Reagent grade or equivalent is required.

5.4.1.14 Methylene Chloride: methylene chloride (suitable for residue and pesticide analysis, GC/MS, HPLC, GC, Spectrophotometry or equivalent) is required for cleaning the aqueous acidic DNPH solution, rinsing glassware, and recovery of sample trains.

5.4.1.15 Cyclohexane: cyclohexane (HPLC grade) is required for cleaning the aqueous acidic DNPH solution.

NOTE: Do not use spectroanalyzed grades of cyclohexane if this sampling methodology is extended to aldehydes and ketones with four or more carbon atoms.

5.4.1.16 Methanol: methanol (HPLC grade or equivalent) is required for rinsing glassware.

5.4.1.17 Acetonitrile: acetonitrile (HPLC grade or equivalent) is required for rinsing glassware.

5.4.1.18 Formaldehyde: Analytical grade or equivalent formaldehyde is required for preparation of standards. If other aldehydes or ketones are used, analytical grade or equivalent is required.

5.4.2 Preparation of Aqueous Acidic DNPH Derivatizing Reagent: Each batch of DNPH reagent should be prepared and purified within five days of sampling, according to the procedure described below.

5.4.2.1 Place an 8-L container under a fume hood on a magnetic stirrer. Add a large stir bar and fill the container half full of HPLC-grade water. Save the empty bottle from HPLC-grade water. Start the stirring bar and adjust the stir rate to be as fast as possible. Using a graduated cylinder, measure 1.4 mL of concentrated hydrochloric acid. Slowly pour the acid into the stirring water. Fumes may be generated and the water may become warm. Weigh the DNPH crystals on a one-place balance (see Table 1 for approximate amounts) and add to the stirring acid solution. Fill the 8 L container to the 8 L mark with HPLC water and stir overnight. If all of the DNPH crystals have dissolved overnight, add additional DNPH and stir for two more hours. Continue the process of adding DNPH with additional stirring until a saturated solution has been formed. Filter the DNPH solution using vacuum filtration. Gravity filtration may be used, but a

much longer time is required. Store the filtered solution in an amber bottle at room temperature.

TABLE 1. APPROXIMATE AMOUNT OF CRYSTALLINE DNPH USED
TO PREPARE A SATURATED SOLUTION

Amount of Moisture in DNPH	Weight Required per 8 L of Solution
10 weight percent	31 g
15 weight percent	33 g
30 weight percent	40 g

Within five days of proposed use, place about 1.6 L of the DNPH reagent in a 2 L separatory funnel. Add approximately 200 mL of methylene chloride and stopper the funnel. Wrap the stopper of the funnel with paper towels to absorb any leakage. Invert and vent the funnel. Then shake vigorously for 3 minutes. Initially, the funnel should be vented frequently (every 10 - 15 sec). After the layers have separated, discard the lower (organic) layer.

Extract the DNPH a second time with methylene chloride and finally with cyclohexane. When the cyclohexane layer has separated from the DNPH reagent, the cyclohexane layer will be the top layer in the separatory funnel. Drain the lower layer (the cleaned extracted DNPH reagent solution) into an amber bottle that has been rinsed with acetonitrile and allowed to dry.

5.4.3 Quality Control: Take two aliquots of the extracted DNPH reagent. The size of the aliquots is dependent upon the exact sampling procedure used, but 100 mL is reasonably representative. To ensure that the background in the reagent is acceptable for field use, analyze one aliquot of the reagent according to the procedure of EPA Draft Method 8315. Save the other aliquot of aqueous acidic DNPH for use as a method blank when the analysis is performed.

5.4.4 Shipment to the Field: Tightly cap the bottle containing extracted DNPH reagent using a Teflon®-lined cap. Seal the bottle with Teflon® tape. After the bottle is labeled, the bottle may be placed in a friction-top can (paint can or equivalent) containing a 1 -2 inch layer of granulated charcoal and stored at ambient temperature until use.

If the DNPH reagent has passed the Quality Control criteria, the reagent may be packaged to meet necessary shipping requirements and sent to the sampling area. If the Quality Control criteria are not met, the reagent solution may be re-extracted or the solution may be re-prepared and the extraction sequence repeated.

If the DNPH reagent is not used in the field within five days of extraction, an aliquot may be taken and analyzed as described Draft Method 8315. If the reagent meets the Quality Control requirements, the reagent may be used. If the reagent does not meet Quality Control requirements, the reagent must be discarded and new reagent must be prepared and tested.

5.4.5 Calculation of Acceptable Levels of Impurities in DNPH Reagent: The acceptable impurity level (AIL, µg/mL) is calculated from the expected analyte level in the sampled gas (EAL, ppbv), the volume of air that will be sampled at standard conditions (SVOL, L), the formula weight of the analyte (FW, g/mol), and the volume of DNPH reagent that will be used in the impingers (RVOL, mL):

$$AIL = 0.1 \times [EAL \times SVOL \times FW / 22.4 \times (FW + 180) / FW] / (RVOL \times 1000).$$

where 0.1 is the acceptable contaminant level, 22.4 is a factor relating ppbv to g/L, 180 is a factor relating the underivatized analyte to the derivatized analyte, and 1000 is a unit conversion factor.

5.4.6 Disposal of Excess DNPH Reagent: Excess DNPH reagent may be returned to the laboratory and recycled or treated as aqueous waste for disposal purposes. 2,4-Dinitrophenylhydrazine is a flammable solid when dry so water should not be evaporated from the solution of the reagent.

5.5 Field Spike Standard Preparation: To prepare a formaldehyde field spiking standard at 4.01 mg/mL, use a 500µL syringe to transfer 0.5 mL of 37% by weight of formaldehyde (401 mg/mL) to a 50 mL volumetric flask containing approximately 40 mL of methanol. Dilute to 50 mL with methanol.

6.0 SAMPLE COLLECTION, PRESERVATION, AND HANDLING

6.1 Because of the complexity of this method, field personnel should be trained in and experienced with the test procedures in order to obtain reliable results.

6.2 Laboratory Preparation:

6.2.1 All the components shall be maintained and calibrated according to the procedure described in APTD-0576, unless otherwise specified.

6.2.2 Weigh several 200- to 300-g portions of silica gel in airtight containers to the nearest 0.5 g. Record on each container the total weight of the silica gel plus containers. As an alternative to preweighing the silica gel, it may instead be weighed directly in the impinger or sampling holder just prior to train assembly.

6.3 Preliminary Field Determinations:

6.3.1 Select the sampling site and the minimum number of sampling points according to EPA Method 1 or other relevant criteria. Determine the stack pressure, temperature, and range of velocity heads using EPA Method 2. A leak-check of the pitot lines according to EPA Method 2, Section 3.1, must be performed. Determine the stack gas moisture content using EPA Approximation Method 4 or its alternatives to establish estimates of isokinetic sampling-rate settings. Determine the stack gas dry molecular weight, as described in EPA Method 2, Section 3.6. If integrated EPA Method 3 sampling is used for molecular weight determination, the integrated bag sample shall be taken simultaneously with, and for the same total length of time as, the sample run.

6.3.2 Select a nozzle size based on the range of velocity heads so that it is not necessary to change the nozzle size in order to maintain isokinetic sampling rates below 28 L/min (1.0 cfm). During the run, do not change the nozzle.

Ensure that the proper differential pressure gauge is chosen for the range of velocity heads encountered (see Section 2.2 of EPA Method 2).

6.3.3 Select a suitable probe liner and probe length so that all traverse points can be sampled. For large stacks, to reduce the length of the probe, consider sampling from opposite sides of the stack.

6.3.4 A minimum of 45 ft³ of sample volume is required for the determination of the Destruction and Removal Efficiency (DRE) of formaldehyde from incineration systems (45ft³ is equivalent to one hour of sampling at 0.75 dscf). Additional sample volume shall be collected as necessitated by the capacity of the DNPH reagent and analytical detection limit constraints. To determine the minimum sample volume required, refer to sample calculations in Section 10.

6.3.5 Determine the total length of sampling time needed to obtain the identified minimum volume by comparing the anticipated average sampling rate with the volume requirement. Allocate the same time to all traverse points defined by EPA Method 1. To avoid timekeeping errors, the length of time sampled at each traverse point should be an integer or an integer plus 0.5 min.

6.3.6 In some circumstances (e.g., batch cycles) it may be necessary to sample for shorter times at the traverse points and to obtain smaller gas-volume samples. In these cases, careful documentation must be maintained in order to allow accurate calculation of concentrations.

6.4 Preparation of Collection Train:

6.4.1 During preparation and assembly of the sampling train, keep all openings where contamination can occur covered with Teflon® film or aluminum foil until just prior to assembly or until sampling is about to begin.

6.4.2 Place 100 mL of cleaned DNPH solution in each of the first two impingers, and leave the third impinger empty. If additional capacity is required for high expected concentrations of formaldehyde in the stack gas, 200 mL of DNPH per impinger may be used or additional impingers may be used for sampling. Transfer approximately 200 to 300 g of pre-weighed silica gel from its container to the fourth impinger. Care should be taken to ensure that the silica gel is not entrained and carried out from the impinger during sampling. Place the silica gel container in a clean place for later use in the sample recovery. Alternatively, the weight of the silica gel plus impinger may be determined to the nearest 0.5 g and recorded.

6.4.3 With a glass or quartz liner, install the selected nozzle using a Viton-A O-ring when stack temperatures are <260°C (500°F) and a woven glass-fiber gasket when temperatures are higher. See APTD-0576 (Rom, 1972) for details. Other connecting systems utilizing either 316 stainless steel or Teflon® ferrules may be used. Mark the probe with heat-resistant tape or by some other method to denote the proper distance into the stack or duct for each sampling point.

6.4.4 Assemble the train as shown in Figure 1. During assembly, do not use any silicone grease on ground-glass joints upstream of the impingers. Use Teflon® tape, if required. A very light coating of silicone grease may be used on ground-glass joints downstream of the impingers, but the silicone grease should be limited to the outer portion (see APTD-0576) of the ground-glass joints to

minimize silicone grease contamination. If necessary, Teflon® tape may be used to seal leaks. Connect all temperature sensors to an appropriate potentiometer/display unit. Check all temperature sensors at ambient temperature.

6.4.5 Place crushed ice all around the impingers. . .

6.4.6 Turn on and set the probe heating system at the desired operating temperature. Allow time for the temperature to stabilize.

6.5 Leak-Check Procedures:

6.5.1 Pre-test Leak Check:

6.5.1.1 After the sampling train has been assembled, turn on and set the probe heating system at the desired operating temperature. Allow time for the temperature to stabilize. If a Viton-A O-ring or other leak-free connection is used in assembling the probe nozzle to the probe liner, leak-check the train at the sampling site by plugging the nozzle and pulling a 381-mm Hg (15 in Hg) vacuum.

NOTE: A lower vacuum may be used, provided that the lower vacuum is not exceeded during the test.

6.5.1.2 If an asbestos string is used, do not connect the probe to the train during the leak check. Instead, leak-check the train by first attaching a carbon-filled leak check impinger to the inlet and then plugging the inlet and pulling a 381-mm Hg (15 in Hg) vacuum. (A lower vacuum may be used if this lower vacuum is not exceeded during the test.) Then connect the probe to the train and leak-check at about 25 mm Hg (1 in Hg) vacuum. Alternatively, leak-check the probe with the rest of the sampling train in one step at 381 mm Hg (15 in Hg) vacuum. Leakage rates in excess of 4% of the average sampling rate or >0.00057 m³/min (0.02 cfm), whichever is less, are acceptable.

6.5.1.3 The following leak check instructions for the sampling train described in APTD-0576 and APTD-0581 may be helpful. Start the pump with the fine-adjust valve fully open and coarse-adjust valve completely closed. Partially open the coarse-adjust valve and slowly close the fine-adjust valve until the desired vacuum is reached. Do not reverse direction of the fine-adjust valve, as liquid will back up into the train. If the desired vacuum is exceeded, either perform the leak check at this higher vacuum or end the leak check, as shown below, and start over.

6.5.1.4 When the leak check is completed, first slowly remove the plug from the inlet to the probe. When the vacuum drops to 127 mm (5 in) Hg or less, immediately close the coarse-adjust valve. Switch off the pumping system and reopen the fine-adjust valve. Do not reopen the fine-adjust valve until the coarse-adjust valve has been closed to prevent the liquid in the impingers from being forced backward into the sampling line and silica gel from being entrained backward into the third impinger.

6.5.2 Leak Checks During Sampling Runs:

6.5.2.1 If, during the sampling run, a component change (i.e., impinger) becomes

necessary, a leak check shall be conducted immediately after the interruption of sampling and before the change is made. The leak check shall be done according to the procedure described in Section 6.5.1, except that it shall be done at a vacuum greater than or equal to the maximum value recorded up to that point in the test. If the leakage rate is found to be no greater than 0.00057 m³/min (0.02 cfm) or 4% of the average sampling rate (whichever is less), the results are acceptable. If a higher leakage rate is obtained, the tester must void the sampling run.

NOTE: Any correction of the sample volume by calculation reduces the integrity of the pollutant concentration data generated and must be avoided.

6.5.2.2 Immediately after a component change and before sampling is re-initiated, a leak check similar to a pre-test leak check must also be conducted.

6.5.3 Post-test Leak Check:

6.5.3.1 A leak check is mandatory at the conclusion of each sampling run. The leak check shall be done with the same procedures as the pre-test leak check, except that the post-test leak check shall be conducted at a vacuum greater than or equal to the maximum value reached during the sampling run. If the leakage rate is found to be no greater than 0.00057 m³/min (0.02 cfm) or 4% of the average sampling rate (whichever is less), the results are acceptable. If, however, a higher leakage rate is obtained, the tester shall record the leakage rate and void the sampling run.

6.6 Sampling Train Operation:

6.6.1 During the sampling run, maintain an isokinetic sampling rate to within 10% of true isokinetic, below 28 L/min (1.0 cfm). Maintain a temperature around the probe of 120° ± 14°C (248° ± 25°F).

6.6.2 For each run, record the data on a data sheet such as the one shown in Figure 2. Be sure to record the initial dry-gas meter reading. Record the dry-gas meter readings at the beginning and end of each sampling time increment, when changes in flow rates are made, before and after each leak check, and when sampling is halted. Take other readings required by Figure 2 at least once at each sample point during each time increment and additional readings when significant adjustments (20% variation in velocity head readings) necessitate additional adjustments in flow rate. Level and zero the manometer. Because the manometer level and zero may drift due to vibrations and temperature changes, make periodic checks during the traverse.

6.6.3 Clean the stack access ports prior to the test run to eliminate the chance of sampling deposited material. To begin sampling, remove the nozzle cap, verify that the filter and probe heating systems are at the specified temperature, and verify that the pitot tube and probe are properly positioned. Position the nozzle at the first traverse point, with the tip pointing directly into the gas stream. Immediately start the pump and adjust the flow to isokinetic conditions. Nomographs, which aid in the rapid adjustment of the isokinetic sampling rate without excessive computations, are available. These nomographs are designed for use when the Type S pitot tube coefficient is 0.84 ± 0.02 and the stack gas equivalent density (dry molecular weight) is equal to 29 ± 4. APTD-0576 details the procedure for using the nomographs. If the stack gas molecular weight and

the pitot tube coefficient are outside the above ranges, do not use the nomographs unless appropriate steps are taken to compensate for the deviations.

6.6.4 When the stack is under significant negative pressure (equivalent to the height of the impinger stem), take care to close the coarse-adjust valve before inserting the probe into the stack in order to prevent liquid from backing up through the train. If necessary, the pump may be turned on with the coarse-adjust valve closed.

6.6.5 When the probe is in position, block off the openings around the probe and stack access port to prevent unrepresentative dilution of the gas stream.

6.6.6 Traverse the stack cross section, as required by EPA Method 1, being careful not to bump the probe nozzle into the stack walls when sampling near the walls or when removing or inserting the probe through the access port, in order to minimize the chance of extracting deposited material.

6.6.7 During the test run, make periodic adjustments to keep the temperature around the probe at the proper levels. Add more ice and, if necessary, salt, to maintain a temperature of $<20^{\circ}\text{C}$ (68°F) at the silica gel outlet. Also, periodically check the level and zero of the manometer.

6.6.8 A single train shall be used for the entire sampling run, except in cases where simultaneous sampling is required in two or more separate ducts or at two or more different locations within the same duct, or in cases where equipment failure necessitates a change of trains. An additional train or additional trains may also be used for sampling when the capacity of a single train is exceeded.

6.6.9 When two or more trains are used, separate analyses of components from each train shall be performed. If multiple trains have been used because the capacity of a single train would be exceeded, first impingers from each train may be combined, and second impingers from each train may be combined.

6.6.10 At the end of the sampling run, turn off the coarse-adjust valve, remove the probe and nozzle from the stack, turn off the pump, record the final dry gas meter reading, and conduct a post-test leak check. Also, leak check the pitot lines as described in EPA Method 2. The lines must pass this leak check in order to validate the velocity-head data.

6.6.11 Calculate percent isokineticity (see Method 2) to determine whether the run was valid or another test should be made.

7.0 SAMPLE RECOVERY

7.1 Preparation:

7.1.1 Proper cleanup procedure begins as soon as the probe is removed from the stack at the end of the sampling period. Allow the probe to cool. When the probe can be handled safely, wipe off all external particulate matter near the tip of the probe nozzle and place a cap over the tip to prevent losing or gaining particulate matter. Do not cap the probe tip tightly while the sampling train is cooling because a vacuum will be created, drawing liquid from the impingers back through the sampling train.

7.1.2 Before moving the sampling train to the cleanup site, remove the probe from the sampling train and cap the open outlet, being careful not to lose any condensate that might be present. Remove the umbilical cord from the last impinger and cap the impinger. If a flexible line is used, let any condensed water or liquid drain into the impingers. Cap off any open impinger inlets and outlets. Ground glass stoppers, Teflon® caps, or caps of other inert materials may be used to seal all openings.

7.1.3 Transfer the probe and impinger assembly to an area that is clean and protected from wind so that the chances of contaminating or losing the sample are minimized.

7.1.4 Inspect the train before and during disassembly, and note any abnormal conditions.

7.1.5 Save a portion of all washing solutions (methylene chloride, water) used for cleanup as a blank. Transfer 200 mL of each solution directly from the wash bottle being used and place each in a separate, pre-labeled sample container.

7.2 Sample Containers:

7.2.1 Container 1: Probe and Impinger Catches. Using a graduated cylinder, measure to the nearest mL, and record the volume of the solution in the first three impingers. Alternatively, the solution may be weighed to the nearest 0.5 g. Include any condensate in the probe in this determination. Transfer the impinger solution from the graduated cylinder into the amber flint glass bottle. Taking care that dust on the outside of the probe or other exterior surfaces does not get into the sample, clean all surfaces to which the sample is exposed (including the probe nozzle, probe fitting, probe liner, first impinger, and impinger connector) with methylene chloride. Use less than 500 mL for the entire wash (250 mL would be better, if possible). Add the washings to the sample container.

7.2.1.1 Carefully remove the probe nozzle and rinse the inside surface with methylene chloride from a wash bottle. Brush with a Teflon® bristle brush, and rinse until the rinse shows no visible particles or yellow color, after which make a final rinse of the inside surface. Brush and rinse the inside parts of the Swagelok® fitting with methylene chloride in a similar way.

7.2.1.2 Rinse the probe liner with methylene chloride. While squirting the methylene chloride into the upper end of the probe, tilt and rotate the probe so that all inside surfaces will be wetted with methylene chloride. Let the methylene chloride drain from the lower end into the sample container. The tester may use a funnel (glass or polyethylene) to aid in transferring the liquid washes to the container. Follow the rinse with a Teflon® brush. Hold the probe in an inclined position, and squirt methylene chloride into the upper end as the probe brush is being pushed with a twisting action through the probe. Hold the sample container underneath the lower end of the probe, and catch any methylene chloride, water, and particulate matter that is brushed from the probe. Run the brush through the probe three times or more. With stainless steel or other metal probes, run the brush through in the above prescribed manner at least six times since there may be small crevices in which particulate matter can be entrapped. Rinse the brush with methylene chloride or water, and quantitatively collect these washings in the sample container. After the brushings, make a final rinse

of the probe as described above.

NOTE: Two people should clean the probe in order to minimize sample losses. Between sampling runs, brushes must be kept clean and free from contamination.

7.2.1.3 Rinse the inside surface of each of the first three impingers (and connecting tubing) three separate times. Use a small portion of methylene chloride for each rinse, and brush each surface to which sample is exposed with a Teflon® bristle brush to ensure recovery of fine particulate matter. Water will be required for the recovery of the impingers in addition to the specified quantity of methylene chloride. There will be at least two phases in the impingers. This two-phase mixture does not pour well, and a significant amount of the impinger catch will be left on the walls. The use of water as a rinse makes the recovery quantitative. Make a final rinse of each surface and of the brush, using both methylene chloride and water.

7.2.1.4 After all methylene chloride and water washings and particulate matter have been collected in the sample container, tighten the lid so that solvent, water, and DNPH reagent will not leak out when the container is shipped to the laboratory. Mark the height of the fluid level to determine whether leakage occurs during transport. Seal the container with Teflon® tape. Label the container clearly to identify its contents.

7.2.1.5 If the first two impingers are to be analyzed separately to check for breakthrough, separate the contents and rinses of the two impingers into individual containers. Care must be taken to avoid physical carryover from the first impinger to the second. The formaldehyde hydrazone is a solid which floats and froths on top of the impinger solution. Any physical carryover of collected moisture into the second impinger will invalidate a breakthrough assessment.

7.2.2 Container 2: Sample Blank. Prepare a blank by using an amber flint glass container and adding a volume of DNPH reagent and methylene chloride equal to the total volume in Container 1. Process the blank in the same manner as Container 1.

7.2.3 Container 3: Silica Gel. Note the color of the indicating silica gel to determine whether it has been completely spent and make a notation of its condition. The impinger containing the silica gel may be used as a sample transport container with both ends sealed with tightly fitting caps or plugs. Ground-glass stoppers or Teflon® caps may be used. The silica gel impinger should then be labeled, covered with aluminum foil, and packaged on ice for transport to the laboratory. If the silica gel is removed from the impinger, the tester may use a funnel to pour the silica gel and a rubber policeman to remove the silica gel from the impinger. It is not necessary to remove the small amount of dust particles that may adhere to the impinger wall and are difficult to remove. Since the gain in weight is to be used for moisture calculations, do not use water or other liquids to transfer the silica gel. If a balance is available in the field, the spent silica gel (or silica gel plus impinger) may be weighed to the nearest 0.5 g.

7.2.4 Sample containers should be placed in a cooler, cooled by although not in contact with ice. Sample containers must be placed vertically and, since they are glass, protected from breakage during shipment. Samples should be cooled during shipment so they will be received cold at the laboratory.

8.0 CALIBRATION

8.1 Probe Nozzle: Probe nozzles shall be calibrated before their initial use in the field. Using a micrometer, measure the inside diameter of the nozzle to the nearest 0.025 mm (0.001 in). Make measurements at three separate places across the diameter and obtain the average of the measurements. The difference between the high and low numbers shall not exceed 0.1 mm (0.004 in). When the nozzles become nicked or corroded, they shall be replaced and calibrated before use. Each nozzle must be permanently and uniquely identified.

8.2 Pitot tube: The Type S pitot tube assembly shall be calibrated according to the procedure outlined in Section 4 of EPA Method 2, or assigned a nominal coefficient of 0.84 if it is not visibly nicked or corroded and if it meets design and intercomponent spacing specifications.

8.3 Metering system:

8.3.1 Before its initial use in the field, the metering system shall be calibrated according to the procedure outlined in APTD-0576. Instead of physically adjusting the dry-gas meter dial readings to correspond to the wet-test meter readings, calibration factors may be used to correct the gas meter dial readings mathematically to the proper values. Before calibrating the metering system, it is suggested that a leak check be conducted. For metering systems having diaphragm pumps, the normal leak check procedure will not detect leakages within the pump. For these cases, the following leak check procedure will apply: make a ten-minute calibration run at 0.00057 m³/min (0.02 cfm). At the end of the run, take the difference of the measured wet-test and dry-gas meter volumes and divide the difference by 10 to get the leak rate. The leak rate should not exceed 0.00057 m³/min (0.02 cfm).

8.3.2 After each field use, check the calibration of the metering system by performing three calibration runs at a single intermediate orifice setting (based on the previous field test). Set the vacuum at the maximum value reached during the test series. To adjust the vacuum, insert a valve between the wet-test meter and the inlet of the metering system. Calculate the average value of the calibration factor. If the calibration has changed by more than 5%, recalibrate the meter over the full range of orifice settings, as outlined in APTD-0576.

8.3.3 Leak check of metering system: The portion of the sampling train from the pump to the orifice meter (see Figure 1) should be leak-checked prior to initial use and after each shipment. Leakage after the pump will result in less volume being recorded than is actually sampled. Use the following procedure: Close the main valve on the meter box. Insert a one-hole rubber stopper with rubber tubing attached into the orifice exhaust pipe. Disconnect and vent the low side of the orifice manometer. Close off the low side orifice tap. Pressurize the system to 13 - 18 cm (5 - 7 in) water column by blowing into the rubber tubing. Pinch off the tubing and observe the manometer for 1 min. A loss of pressure on the manometer indicates a leak in the meter box. Leaks must be corrected.

NOTE: If the dry-gas-meter coefficient values obtained before and after a test series differ by >5%, either the test series must be voided or calculations for test series must be performed using whichever meter coefficient value (i.e., before or after) gives the lower value of total sample volume.

8.4 Probe heater: The probe heating system must be calibrated before its initial use in the field according to the procedure outlined in APTD-0576. Probes constructed according to APTD-0581 need not be calibrated if the calibration curves in APTD-0576 are used.

8.5 Temperature gauges: Each thermocouple must be permanently and uniquely marked on the casting. All mercury-in-glass reference thermometers must conform to ASTM E-1 63C or 63F specifications. Thermocouples should be calibrated in the laboratory with and without the use of extension leads. If extension leads are used in the field, the thermocouple readings at ambient air temperatures, with and without the extension lead, must be noted and recorded. Correction is necessary if the use of an extension lead produces a change $>1.5\%$.

8.5.1 Impinger and dry-gas meter thermocouples: For the thermocouples used to measure the temperature of the gas leaving the impinger train, three-point calibration at ice water, room air, and boiling water temperatures is necessary. Accept the thermocouples only if the readings at all three temperatures agree to $\pm 2^{\circ}\text{C}$ (3.6°F) with those of the absolute value of the reference thermometer.

8.5.2 Probe and stack thermocouple: For the thermocouples used to indicate the probe and stack temperatures, a three-point calibration at ice water, boiling water, and hot oil bath temperatures must be performed. Use of a point at room air temperature is recommended. The thermometer and thermocouple must agree to within 1.5% at each of the calibration points. A calibration curve (equation) may be constructed (calculated) and the data extrapolated to cover the entire temperature range suggested by the manufacturer.

8.6 Barometer: Adjust the barometer initially and before each test series to agree to within ± 2.5 mm Hg (0.1 in Hg) of the mercury barometer or the corrected barometric pressure value reported by a nearby National Weather Service Station (same altitude above sea level).

8.7 Triple-beam balance: Calibrate the triple-beam balance before each test series, using Class S standard weights. The weights must be within $\pm 0.5\%$ of the standards, or the balance must be adjusted to meet these limits.

9.0 CALCULATIONS

Carry out calculations, retaining at least one extra decimal figure beyond that of the acquired data. Round off figures after final calculation.

9.1 Calculation of Total Formaldehyde:

To determine the total formaldehyde in mg, use the following equation:

Total mg formaldehyde = $C_d \times V \times DF \times$

$([g/mole \text{ aldehyde}]/[g/mole \text{ DNPH derivative}]) \times$

$10^{-3} \text{ mg}/\mu\text{g}$

where:

C_d = measured concentration of DNPH-formaldehyde derivative, $\mu\text{g}/\text{mL}$.

V = organic extract volume, mL

DF = dilution factor

9.2 Formaldehyde concentration in stack gas:

Determine the formaldehyde concentration in the stack gas using the following equation:

$$C_f = K [\text{total formaldehyde, mg}] / V_{m(\text{std})}$$

where:

$K = 35.31 \text{ ft}^3/\text{m}^3$ if $V_{m(\text{std})}$ is expressed in English units

$= 1.00 \text{ m}^3/\text{m}^3$ if $V_{m(\text{std})}$ is expressed in metric units

$V_{m(\text{std})}$ = volume of gas sample as measured by dry gas meter, corrected to standard conditions, dscm (dscf)

9.3 Average Dry Gas Meter Temperature and Average Orifice Pressure Drop are obtained from the data sheet.

9.4 Dry Gas Volume: Calculate $V_{m(\text{std})}$ and adjust for leakage, if necessary, using the equation in Section 6.3 of EPA Method 5.

9.5 Volume of Water Vapor and Moisture Content: Calculate the volume of water vapor and moisture content from equations 5-2 and 5-3 of EPA Method 5.

10.0 DETERMINATION OF VOLUME TO BE SAMPLED

To determine the minimum sample volume to be collected, use the following sequence of equations.

10.1 From prior analysis of the waste feed, the concentration of formaldehyde (FORM) introduced into the combustion system can be calculated. The degree of destruction and removal efficiency that is required is used to determine the maximum amount of FORM allowed to be present in the effluent. This amount may be expressed as:

Max FORM₁ Mass -

$$[(WF) (FORM_1 \text{ conc}) (100 - \%DRE)] / 100$$

where:

WF - mass flow rate of waste feed per h, g/h (lb/h)

FORM₁ - concentration of FORM (wt %) introduced into the combustion process

DRE - percent Destruction and Removal Efficiency required

Max FORM - mass flow rate (g/h [lb/h]) of FORM emitted from the combustion source

10.2 The average discharge concentration of the FORM in the effluent gas is determined by comparing the Max FORM with the volumetric flow rate being exhausted from the source. Volumetric flow rate data are available as a result of preliminary EPA Method 1 - 4 determinations:

$$\text{Max FORM}_1 \text{ conc} = [\text{Max FORM}_1 \text{ Mass}] / DV_{\text{eff(Std)}}$$

where:

DV_{eff(Std)} - volumetric flow rate of exhaust gas, dscm (dscf)

FORM₁ conc - anticipated concentration of the FORM in the exhaust gas stream, g/dscm (lb/dscf)

10.3 In making this calculation, it is recommended that a safety margin of at least ten be included.

$$[LDL_{\text{FORM}} \times 10] / [FORM_1 \text{ conc}] = V_{\text{tbc}}$$

where:

LDL_{FORM} - detectable amount of FORM in entire sampling train

V_{tbc} - minimum dry standard volume to be collected at dry-gas meter

10.4 The following analytical detection limits and DNPH Reagent Capacity (based on a total volume of 200 mL in two impingers) must also be considered in determining a volume to be sampled.

Table 2. Instrument Detection Limits and Reagent Capacity for Formaldehyde Analysis¹

Analyte	Detection Limit, ppbv ²	Reagent Capacity, ppmv
formaldehyde	1.8	66
acetaldehyde	1.7	70
acrolein	1.5	75
acetone/propionaldehyde	1.5	75
butyraldehyde	1.5	79
methyl ethyl ketone	1.5	79
valeraldehyde	1.5	84
isovaleraldehyde	1.4	84
hexaldehyde	1.3	88
benzaldehyde	1.4	84
o-/m-/p-tolualdehyde	1.3	89
dimethylbenzaldehyde	1.2	93

¹ Oxygenated compounds in addition to formaldehyde are included for comparison with formaldehyde; extension of the methodology to other compounds is possible.

² Detection limits are determined in solvent. These values therefore represent the optimum capability of the methodology.

11.0 QUALITY CONTROL

11.1 Sampling: See EPA Manual 600/4-77-027b for Method 5 quality control.

11.2 Analysis: The quality assurance program required for this method includes the analysis of field and method blanks, procedure validations, and analysis of field spikes. The assessment of combustion data and positive identification and quantitation of formaldehyde are dependent on the integrity of the samples received and the precision and accuracy of the analytical methodology. Quality Assurance procedures for this method are designed to monitor the performance of the analytical methodology and to provide the required information to take corrective action if problems are observed in laboratory operations or in field sampling activities.

11.2.1 Field Blanks: Field blanks must be submitted with the samples collected at each sampling site. The field blanks include the sample bottles containing aliquots of sample recovery solvents, methylene chloride and water, and unused DNPH reagent. At a minimum, one complete sampling train will be assembled in the field staging area, taken to the sampling area, and leak-checked at the beginning and end of the testing (or for the same total number of times as the actual sampling train). The probe of the blank train must be heated during the sample test. The train will be recovered as if it were an actual test sample. No gaseous sample will be passed through the Blank sampling train.

11.2.2 Method Blanks: A method blank must be prepared for each set of analytical operations, to evaluate contamination and artifacts that can be derived from glassware, reagents, and sample handling in the laboratory.

11.2.3 Field Spike: A field spike is performed by introducing 200 μ L of the Field Spike Standard into an impinger containing 200 mL of DNPH solution. Standard impinger recovery procedures are followed and the field spike sample is returned to the laboratory for analysis. The field spike is used as a check on field handling and recovery procedures. An aliquot of the field spike standard is retained in the laboratory for derivatization and comparative analysis.

12.0 METHOD PERFORMANCE

12.1 Method performance evaluation: The following expected method performance parameters for precision, accuracy, and detection limits are provided in Table 3.

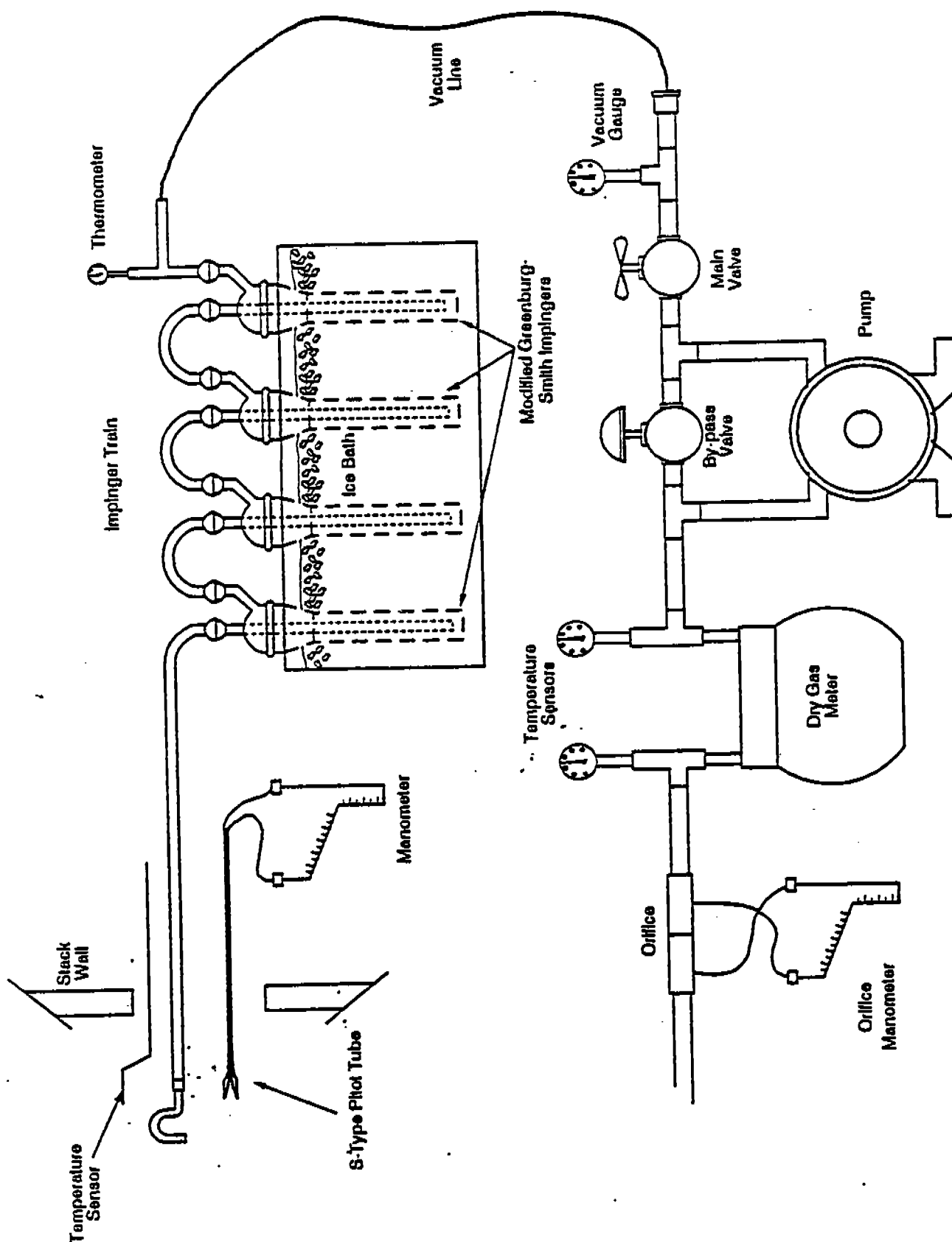
Table 3. Expected Method Performance for Formaldehyde

Parameter	Precision	¹ Accuracy ²	Detection Limit ³
Matrix: Dual trains	$\pm 15\%$ RPD	$\pm 20\%$	1.5×10^{-7} lb/ft ³ (1.8 ppbv)

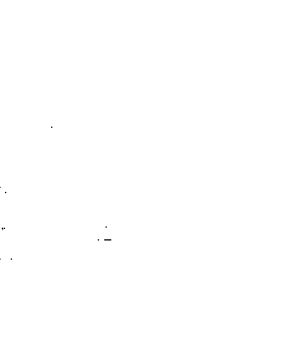
¹ Relative percent difference limit for dual trains.

² Limit for field spike recoveries.

³ The lower reporting limit having less than 1% probability of false positive detection.



Formaldehyde Sampling Train



Static Pressure, mm Hg (in. Hg) _____

Filter No. _____

[illegible]

Figure 2. Field Data Sheet

DRAFT

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It has not been formally released by EPA
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to represent Agency policy. It is being
circulated for comment on its technical
accuracy and for any clarifications.

FIELD TEST OF A GENERIC METHOD FOR SAMPLING AND ANALYSIS OF ISOCYANATES

Interim Report
(Work Assignment 55)

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July 1993

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accuracy and policy implications.

DISCLAIMER

The information in this document has been funded wholly by the United States Environmental Protection Agency under EPA Contract Number 68-D1-0010 to Radian. It has been subjected to the Agency's peer and administrative review, and it has been approved for publication as an EPA document. Mention of trade names or commercial products does not constitute endorsement or recommendation for use.

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EXECUTIVE SUMMARY

Isocyanates are used extensively in the production of polyurethane materials such as flexible foam, enamel wire coatings, paint formulations and in binders for the pressed board industry. Because of their widespread use and known adverse physiological effects, several isocyanates have been listed in Title III of the Clean Air Act Amendments of 1990. The isocyanates of interest are: 2,4-toluene diisocyanate (TDI), methylene diphenyl diisocyanate (MDI), 1,6-hexamethylene diisocyanate (HDI) and methyl isocyanate (MI). Previously, no validated sampling and analytical methodology for these compounds relative to stationary sources existed.

The field validation study presented in this report is a culmination of laboratory investigations, performed under previous work assignments, which were designed to develop and evaluate a viable approach for the determination of isocyanate emissions from stationary sources. After the successful completion of the laboratory studies, the sampling and analysis approach was formulated and a field validation test was initiated. At the direction of the EPA, TDI was selected as the primary analyte.

The test site selected was a flexible foam manufacturing facility in High Point, North Carolina, which used TDI in the manufacturing process. The approximate level of TDI in the emission stream was determined by the analysis of samples collected during a presurvey. A sampling scheme was then designed to ensure the collection of sufficient samples to yield statistically valid data. Following the EPA Method 301 protocol, quadruplicate trains (QUAD) were operated simultaneously with four co-located probes. Two of the trains were spiked with TDI and two were unspiked. Samples from eight QUAD runs (minimum of six valid runs required by Method 301) were returned to the laboratory and analyzed according to the analytical procedure developed in laboratory studies. These data were statistically evaluated following Method 301 protocol to determine the performance of the method relative to bias and precision. These results are summarized in the following table. The precision for both the spiked and unspiked trains was less than 5% RSD, which is well within the precision criteria (% RSD < 50)

Method Validation Statistical Summary

Precision ^a	
% RSD for Spiked Samples	3.55 ^b
% RSD for Unspiked Samples	4.72 ^b
Accuracy ^a	
Bias:	-295 μ g
Significant?	No
Correction Factor	1.0 ^c
Recovery ^a	
Amount Spiked (as TDI)	7828 μ g
Average Percent Recovered	95

^aResults are based on the average of seven QUAD runs (14 spiked trains and 14 unspiked trains). TDI was present in the stack emissions and was therefore collected as background in the unspiked trains as well as in the spiked trains.

^bEPA Method 301 requires the precision to be <50% RSD for the method to be acceptable.

^cEPA Method 301 requires the calculated Correction Factor to be between 0.7 and 1.3 for the method to be acceptable.

for an acceptable method as tested. Using the data from all eight runs, the bias was found to be significant at the 95% level of confidence thus requiring the use of a correction factor of 1.053. Using the data from only seven runs (eliminating run number eight due to a questionable leak check for one of the trains) the bias was not significant and therefore did not require the calculation of a correction factor. In either case, the method was well within the bias acceptance criteria (correction factor between 0.7 and 1.3) for an acceptable method as tested.

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INTRODUCTION

Sampling and analytical methods for a particular analyte or group of analytes can be evaluated and validated by demonstrating their performance in field tests, thereby establishing the precision and bias of the methods experimentally. Few methods have been fully validated for sampling and analyzing the organic compounds listed in Title III of the Clean Air Act Amendments of 1990. For some analytes, methods have been validated for sample analysis, but not for sample collection. Full validation for both sampling and analytical methods, for both field and laboratory operations, is available for fewer than 10 percent of the analytes listed in Title III of the Clean Air Act Amendments at any source category. Field validation may be performed by side-by-side comparison of a candidate method to a validated method to establish comparable performance for the same analytes in the same matrix (same source category). Another procedure for validation of a method is to spike known quantities of analytes into the collection apparatus in the field so that the precision and bias of the method can be demonstrated from sample collection through analysis.

EPA, under the authority of Title III of the Clean Air Act Amendments (CAAA) of 1990, requires the identification and validation of sampling and analytical methods for the isocyanate compounds which are listed among the 189 hazardous air pollutants identified in Title III. These isocyanate compounds are listed in Table 1-1. Development of sampling and analytical methods for these four compounds was accomplished under Work Assignments 11, 21, and 40 on EPA Contract No. 68-D1-0010. At the direction of EPA, initial efforts were directed to the measurement of 2,4-toluene diisocyanate (TDI) emissions.

The objective of this work assignment was to validate the isocyanate sampling and analytical test method through field testing at an operating stationary source. The method was validated by collecting flue gas samples for the analysis of 2,4-TDI, and evaluating the data for bias and precision. EPA Method 301, "Field Validation of Pollutant Measurement Methods from Various Waste Media," was used as

Table 1-1

Isocyanates Listed in the Clean Air Act Amendments of 1990

Hexamethylene-1,6-diisocyanate (HDI)

2,4-Toluene diisocyanate (TDI)*

Methylene diphenyl diisocyanate (MDI)

Methyl isocyanate (MI)

***The 2,6 TDI isomer may also be present but is not listed in the CAAA.**

a model for the validation protocol. Analyte spiking was used with quadruplicate sampling trains to generate the required data. The field validation was performed at an industrial facility which manufactures flexible foam products. Only two of the quadruplicate trains were spiked for each run. The two unspiked trains were used to establish the background level of target compound in the stack gas.

The sampling method utilizes a Method 5-type sampling train, which operates with a solution of 1-(2-pyridyl) piperazine and toluene in the impingers. Stack gas is extracted from the source through a heated probe and drawn through the impingers. TDI present in the stack gas reacts with the piperazine to form an isocyanate derivative. The quantity of isocyanate is determined by solvent exchange of the toluene solution with acetonitrile followed by high pressure liquid chromatographic (HPLC) analysis.

This report discusses the details of the field validation study. Section 2.0, Conclusions and Recommendations, summarizes the results and provides recommendations for future work. Sections 3.0 and 4.0 provide details of the sampling and analysis procedures respectively. Section 5.0 is a detailed discussion of the procedures, calculations and quality control.

CONCLUSIONS AND RECOMMENDATIONS

Based on the results presented in Section 6.0 of this report, the following conclusions can be made concerning the validity of the method as tested under the conditions described in this report:

- The calculated values for precision (%RSD) for both the spiked and unspiked trains, 3.55 and 4.72 respectively, are both well within the acceptance criteria of less than 50% RSD found in Section 6.3 of the EPA Method 301. Therefore, the method as tested at the source category described meets the precision requirements;
- The method bias, at the concentration levels tested, was found to be significantly different from zero at the 95% level of confidence when the data from all eight runs (minimum of six runs required) were used in the calculations. A correction factor of 1.053 would be required if all eight runs are included in the bias calculation. Good technical reasons exist for excluding one of eight QUAD runs. If this run is eliminated, no bias correction is required. In either case the correction factor is well within the acceptance criteria of 0.7 to 1.3 found in Section 1.2 of the EPA Method 301. Therefore, the method as tested at the source category described meets the bias and correction factor requirements; and
- The method as tested is sufficiently robust to allow testing at sources similar to the source tested in this study where the stack gas moisture is less than 1% by volume, the stack temperature is less than 30 degrees C and the presence of other compounds that may interfere with the analysis are minimal.

Recommendations for future testing and validation of the method for the sampling and analysis of isocyanates include the following:

- Identify a source for testing that has more than one isocyanate present in the stack gas;
- Spike as many of the four CAAA target isocyanates as possible into the train before sampling in order to gain as much information as possible from the field test; and

- Design the condenser between the first and second impinger of the train to more efficiently reduce the loss of toluene from the first impinger and minimize compound breakthrough due entrained aerosols.

3.0

FIELD TEST

The objective of this program was to perform a field test to establish the bias and precision of a sampling and analytical method for isocyanate compounds listed in Title III of the Clean Air Act Amendments of 1990. The method evaluation in this test series resulted from extensive literature reviews, industry consultation and laboratory development. To achieve the test objective, an industrial source with known emissions of TDI was selected as a field test site. Factors in the site selection were easy access, ample space for the quadruple sampling trains and proximity to Radian's office and laboratory in Research Triangle Park, North Carolina.

3.1

Site Description

The field validation test was performed at a flexible foam production plant located in High Point, North Carolina. In the manufacturing process starting materials (TDI, water, a polyether resin, methylene chloride, an amine catalyst, and coloring additives) are blended and continuously fed onto a conveyer belt. The TDI reacts with water and releases CO_2 , which causes foaming in the resin material. Dichloromethane (DCM) can be added as a supplemental "blowing" or foaming agent. The heat from the reaction of TDI and water causes the DCM to vaporize, resulting in increased foaming. The density of the foam is controlled by the amount of TDI, water and DCM added. The foaming action continues as the material proceeds down the conveyer belt. Finished product is then allowed to cure and degas for 24 to 48 hours.

3.2

Sampling Location

Figure 3-1 presents a schematic view of the sampling location. Three induced draft (ID) fans are used to exhaust TDI and DCM vapors from the production process through three separate uninsulated sheet metal ducts that extend through the roof. Two of the ducts are connected by a 30-foot horizontal duct, 34 inches in diameter, which then extends vertically to a height of 25 feet above the roof top. A 6 inch

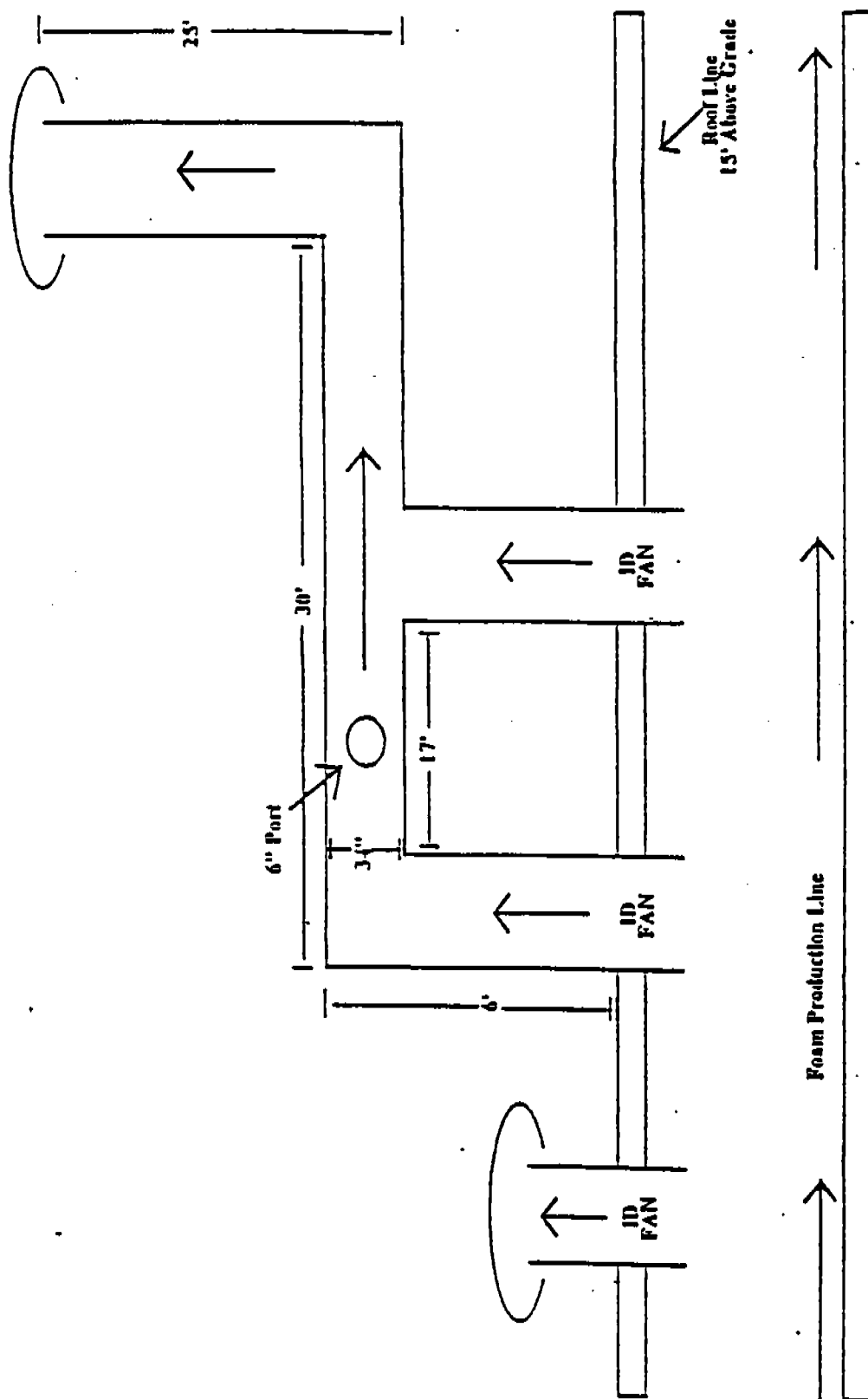


Figure 3-1. Sample Location

diameter sampling port is located in the horizontal duct midway between vertical ducts number 2 and 3, approximately 5 feet above the roof level. The roof level is approximately 15 feet above the ground.

A recovery trailer was located on the ground immediately in front of the sampling area, allowing easy communication between the sampling crew and recovery area. Two-way radio communication between the facility production personnel and the sampling crew allowed coordination between production startup and the start of each sampling run.

3.3 Test Schedule

The recovery trailer and test equipment were mobilized on Saturday, February 20, 1993. Equipment setup took place Saturday afternoon and Sunday, and testing began Monday morning.

The sampling schedule is shown in Table 3-1. Eight runs were completed, which included two extra runs above the required minimum of six.

3.4 Sample Collection

3.4.1 Quad Probe

Sampling was performed by withdrawing stack gas from a single port in the stack through a quad probe, then directing the sampled gas simultaneously to four independently operated sampling trains. The quad probe contains four similar heated sampling probes that were inserted into the stack as one unit, as shown in Figure 3-2. The front end of the quad probe was positioned in the center of the stack and remained

Table 3-1
Test Schedule

Run	Date	Start Time	Stop Time
1	2-22-93	1215	1300
2	2-22-93	1330	1410
3	2-23-93	0945	1085
4	2-23-93	1335	1415
5	2-24-93	1010	1110
6	2-24-93	1335	1420
7	2-25-93	1215	1255
8	2-25-93	1315	1355

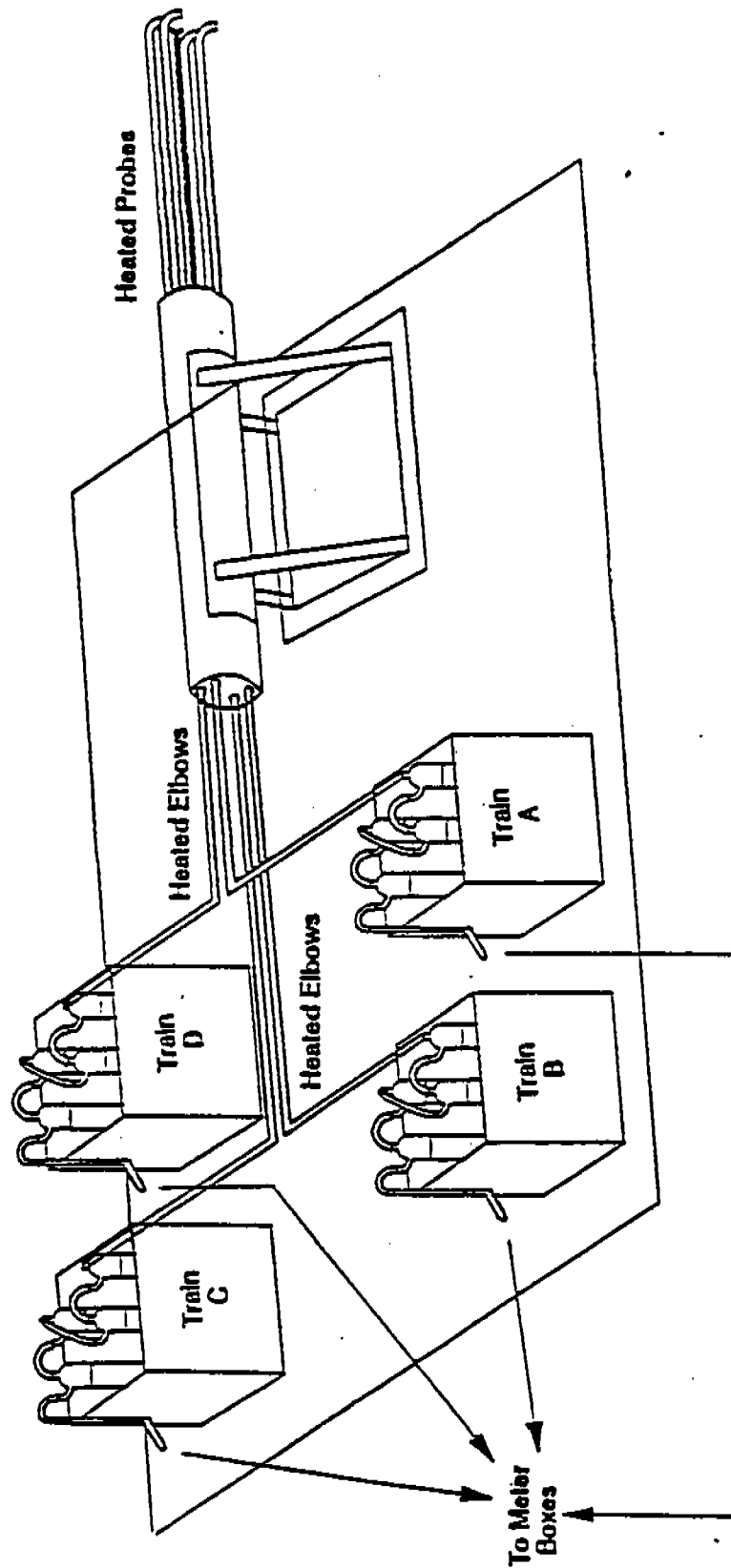


Figure 3-2. Schematic of Quad Train Setup

in that location during each test. The stack was not traversed nor were stack gas velocity measurements made, because determination of the true concentration and emission rate of the target compound in the stack gas was not required to meet the objectives of this program.

Method 301 of 40 CFR Part 63 describes field validation procedures and details the criteria for the quadruple sampling probe tip arrangement. This method requires the inside edge of sampling probe tips to be situated in a 6.0 cm x 6.0 cm square area. The area encompassed by the probe tip arrangement should occupy less than 5% of the stack cross-sectional area. The cross-sectional area of the probe tip arrangement used in this test was 5.8 square inches as measured from the probe/nozzle centerlines. This area is less than 1% of the stack cross-sectional area of 908 square inches, which satisfies the Method 301 criterion.

3.4.2 Quad-Train Assembly

Four independent sampling trains made up the quad-train assembly. Although four meter boxes were required, the velocity head (ΔP) was determined using only one set of pitot tubes. The sampling trains were identified as Train A, B, C, and D. Two of the four trains were spiked before each run. The spiking compound was added to the first impinger of these trains in the field for bias determination. The sampling train test matrix is given in Table 3-2.

3.5 Sampling Preparation

3.5.1 Glassware Preparation

All glassware used for sampling was thoroughly cleaned prior to use. This included the probe, impingers, all sample bottles and all utensils used during sample recovery. All glassware was washed with hot soapy water, rinsed with hot tap water, rinsed with distilled water and baked in an oven at 300 °C for four hours. The glassware

Table 3-2

Sampling Train Test Matrix

Rim #	Train Designation	
	Spiked	Unspiked
1	A, B	C, D
2	C, D	A, B
3	A, B	C, D
4	C, D	A, B
5	A, B	C, D
6	C, D	A, B
7	A, B	C, D
8	C, D	A, B

was then triple-rinsed with HPLC grade acetonitrile, followed by triple-rinsing with HPLC grade toluene. Open ends of glassware were covered with aluminum foil to minimize potential contamination during transportation and set-up.

3.5.2 Preparation of Impinger Absorbing Solution

Historical data available from the host test site facility and data resulting from the collection of preliminary samples by Radian indicated that the concentration of TDI in the process exhaust was 1 ppm or less, depending on the density of foam being produced on any given day. At this concentration, a 30 cubic foot sample size would result in the collection of approximately 7 mg of TDI. Using the reaction stoichiometry of two moles of 1,2-PP per mole of TDI, the piperazine in toluene solution was then prepared at a concentration level three times the calculated minimum needed, or 133 $\mu\text{g/mL}$. This would provide a total of approximately 40 mg of 1,2-PP in 300 mL of impinger solution in the first impinger available for reaction with TDI. At this concentration, approximately 22 mg of TDI could be collected in the first impinger before the reagent was exhausted. This solution was prepared in the laboratory just prior to use in the field, and was used within 10 days of preparation.

3.5.3 Preparation of TDI Spiking Solution

The TDI spiking solution was prepared at a concentration of 1.5 mg of the derivatized TDI per 1 mL of acetonitrile. Fifteen mL of this spiking solution was spiked into the first impinger of two of the four trains prior to each QUAD run. This spiking scheme resulted in a total spike amount of derivatized TDI of 22.5 mg, which is equivalent to 7.83 mg of underivatized TDI. This is an amount equivalent to the amount of TDI expected to be collected in the train from the stack gas based on presurvey samples. Therefore, the amount present in the two spiked trains was designed to be at least twice the amount present in the two unspiked trains.

3.5.4 Sampling Equipment Preparation

Final sampling train preparations included calibration and leak checking of all the train equipment, including meter boxes, thermocouples, nozzles, pitot tubes, and umbilicals. Reference calibration procedures were followed when available, and the results were properly documented and archived. If a referenced calibration technique for a particular piece of apparatus was not available, then a state-of-the-art technique was used. A discussion of the techniques used to calibrate this equipment is presented below.

S-Type Pitot Tube Calibration

The EPA has specified guidelines concerning the construction and geometry of an acceptable S-Type pitot tube. If the specified design and construction guidelines are met, a pitot tube coefficient of 0.84 can be used. Information pertaining to the design and construction of the Type-S pitot tube is presented in detail in Section 4.1.1 of EPA Document 600/4-77027b. Only S-Type pitot tubes meeting the required EPA specifications were used. Pitot tubes were inspected and documented as meeting EPA specifications prior to field sampling.

Sampling Nozzle Calibration

Glass nozzles were used for sampling. All nozzles were thoroughly cleaned, visually inspected for damage, and calibrated according to the procedure outlined in Section 4.4.2 of EPA Document 600/4-77-027b.

Dry Gas Meter Calibration

Dry gas meters (DGMs) were used in the sample trains to measure the sample volume and sampling rate. All DGMs were calibrated to document the volume correction factor prior to the departure of the equipment to the field. Post-test

calibration checks were performed after the equipment was returned to Radian's laboratory. Pre- and post-test calibrations agreed to within 5 percent.

Prior to calibration, a positive pressure leak check of the system was performed using the procedure outlined in Section 4.3.2 of EPA Document 600/4-77-23b. The system was placed under approximately 10 inches of water pressure and an oil manometer was used to determine if the pressure decreased over a one-minute period.

After the sampling console was assembled and leak checked, the pump was allowed to run for 15 minutes to allow the pump and DGM to warm up. The valve was then adjusted to obtain the desired flow rate. For the pre-test calibrations, data were collected at the orifice manometer settings (ΔH) of 0.5, 1.0, 1.5, 2.0, 3.0, and 4.0 inches of water. Gas volumes of 5 ft³ were used for the two lower orifice settings, and volumes of 10 ft³ were used for the higher settings. The individual gas meter correction factors (γ_i) were calculated for each orifice setting and averaged. The method requires that each of the individual correction factors fall within $\pm 2\%$ of the average correction factor or the meter must be cleaned, adjusted, and recalibrated. In addition, Radian requires that the average correction factor be 1.00 ± 1 percent. For the post-test calibration, the meter was calibrated three times at the average orifice setting and vacuum which were used during the actual test.

Dry gas meter calibrations were performed at Radian's laboratory using an American® wet test meter as an intermediate standard. The intermediate standard is calibrated every six months against the EPA spirometer at EPA's Emission Measurement Laboratory in Research Triangle Park (RTP), North Carolina.

3.5.5 - Sampling Operations

Vent gas samples were collected isokinetically from a single sampling point located in the center of the duct. Preliminary information about the stack gas velocity useful in selecting nozzle size and calculating the K-factor was obtained during the

pre-site survey. Prior to testing, a leak check of pitot lines was performed according to EPA Method 2. Oxygen (O_2) and carbon dioxide (CO_2) concentrations were ambient levels as determined by EPA Method 3. The stack gas moisture data was measured by the host facility as the relative humidity.

Preparation of Sampling Train

The four sampling trains for each QUAD run were charged and assembled in the recovery trailer. The impinger buckets were marked as Train A, B, C, or D. Tared impingers were used. Approximately 300 mL of the absorbing reagent was transferred to the first impinger and 200 mL to the second impinger. The first impinger of each train was of a Greenburg-Smith design and all remaining impingers were of the modified Greenburg-Smith design. The third impinger was empty, 200 to 300 g of silica gel was placed in the fourth impinger and 400 g of charcoal was placed in the fifth impinger. A water jacketed condenser was placed between the outlet of the first impinger and the inlet to the second impinger to promote cooling and minimize evaporative losses of toluene from the first impinger. Fifteen (15) mL of the spiking solution was pipetted into the first impinger of Trains A and B. Openings were covered with Teflon® film or aluminum foil after the assembly of the trains.

Final assembly of the sampling trains occurred at the sampling location. The complete train configuration is shown in Figure 3-3. Thermocouples were attached to measure the stack temperature and probe outlet and impinger outlet temperatures. Crushed ice was added to each impinger bucket, and the probe heaters were turned on and allowed to stabilize at $120^\circ \pm 12^\circ C$ ($248^\circ \pm 25^\circ F$).

The isocyanate trains were leak checked before and after each sampling run, as required in EPA Method 5. To leak check the assembled train, the nozzle end was capped off and the sampling train evacuated to a vacuum of 15 inches of Hg. After the system was evacuated and the pump isolated from the train, the volume of gas flowing through the system was timed for 60 seconds. The leak rate is required to be

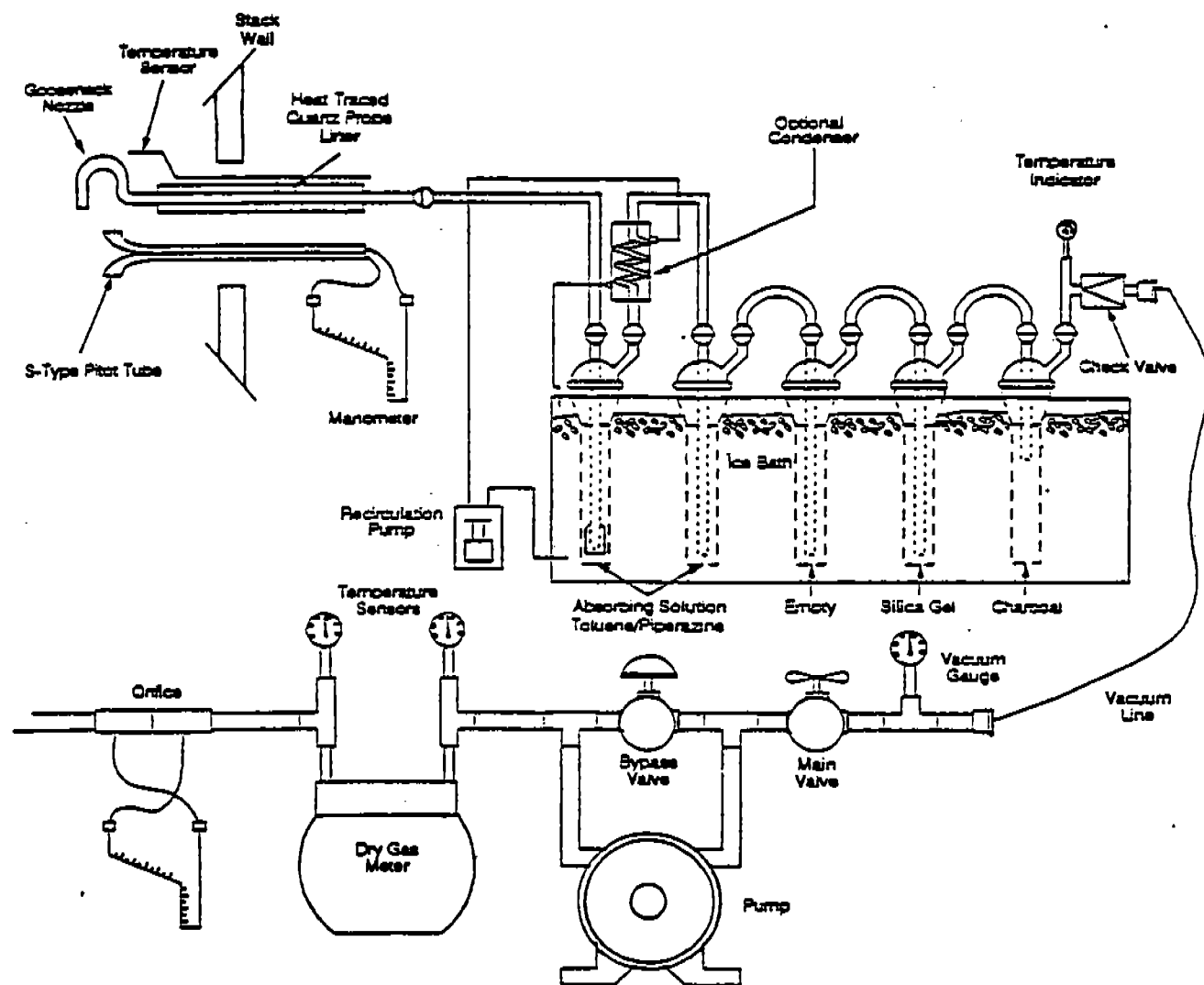


Figure 3-3. Sampling Train for Isocyanate

less than 0.02 acfm or 4% of the average sampling rate, whichever is less. After the leak rate was determined, the cap was slowly removed from the nozzle end until the vacuum in the train returned to atmospheric pressure and then the pump was turned off.

The leak rates and sampling start and stop times were recorded on the sampling task log. Also, any other events that occur during sampling were recorded on the task log (such as pitot cleaning, thermocouple malfunctions, heater malfunctions, and any other unusual occurrences). A nominal sample size of 30 cubic feet was collected in all sampling train. This was accomplished by sampling at a flowrate of 0.5 cubic feet per minute for 60 minutes. The sample volumes for each train by QUAD run are presented in Table 3-3.

3.5.6 Sample Recovery

The sample bottles containing the probe and nozzle washings and the impinger portion of the sampling trains were moved to the recovery trailer.

Each impinger was carefully removed from the impinger bucket, the outside was wiped dry, and the final impinger weight was determined and recorded to calculate stack moisture. The isocyanate sample was then collected in the following two fractions:

- First impinger contents, toluene rinses from the nozzle/probe liner and toluene/acetonitrile rinses of the first impinger and connecting glassware; and
- Contents and toluene/acetonitrile rinses from the second and third impingers and the condenser.

Recovery procedures are detailed in this section. All recovery bottles were wide mouth amber glass with Teflon® lined lids.

Table 3-3.

Quad Train Sample Volumes

Date	Run Number	Train A Vm @ 68° (ft³)	Train B Vm @ 68° (ft³)	Train C Vm @ 68° (ft³)	Train D Vm @ 68° (ft³)
2/22/93	1	33.42	33.89	33.02	33.04
2/22/93	2	29.07	29.65	28.67	28.40
2/23/93	3	34.24	35.15	33.75	33.01
2/23/93	4	30.60	31.17	30.35	29.54
2/24/93	5	34.14	34.70	34.46	32.59
2/24/93	6	35.10	35.17	34.49	33.78
2/25/93	7	31.11	31.94	30.14	29.91
2/25/93	8	30.89	29.73	30.49	31.95

Container 1 - Probe and First Impinger Contents

The contents and rinses of each of the first impingers and first impinger connectors were combined with the corresponding probe/nozzle washing solution. The entire contents of the first impinger were recovered as a single sample, even if two phases were present. The first impinger and connecting tubing were rinsed three times with 15 mL aliquots of toluene. A final rinse of the impinger with acetonitrile was also necessary to remove any water left on the impinger wall and to recover any remaining derivatized TDI.

Container 2 - Second and Third Impinger Contents/Condenser Rinse

The contents and toluene/acetonitrile rinses of the second and third impingers and the condenser of each train were collected in the same manner used for the first impinger described above. The contents of these impingers were analyzed separately from the contents collected in the first impinger to check for breakthrough; therefore, care was taken to avoid physical carryover from the first impinger to the second. The contents of the fourth and fifth impingers were weighed as previously described and then discarded.

Field Blanks

Four field blanks were prepared and recovered during the test, one on each day of testing. The four field blanks were prepared using Trains A, B, C, and D from the two sets of glassware used during the testing. A sampling train was assembled in the staging area, taken to the sampling location, and leak-checked. The probe of the blank train was heated during the generation of the field blank, but no gas sample was passed through the sampling train. The sampling train for the field blank was recovered with the same procedure described for authentic source samples.

Reagent Blank(s)

Aliquots of each lot of toluene, acetonitrile and absorbing reagent were collected daily to be analyzed as reagent blanks.

Sample Storage and Shipping

Sample containers were checked to ensure that complete labels had been affixed. The labels identified Trains A, B, C, or D, as appropriate. Teflon® lids were tightened and secured with Teflon® tape. The sample bottles were stored in a cooler packed with ice and were returned to Radian's laboratory in these coolers at the end of the field test.

3.6 Quality Control

The following quality control measures were implemented during the field testing phase of this program:

- All dry gas meters were calibrated. Calibration procedures were followed for the pitot tube/probe assembly and all thermocouple readout devices.
- Temperatures of the sampling train were maintained at the specified setting ($120 \pm 12^{\circ}\text{C}$) during each sampling run at levels prescribed in the test plan.
- Sampling trains were leak-checked both prior to and after sampling.
- All glassware was washed and oven-baked following appropriate method protocol, given in the test plan.
- All recovery solvents were HPLC grade and an aliquot of each was collected daily as reagent blanks.
- One field blank was collected for every two sampling runs.

- Chain of Custody forms and log books were filled in at the completion of each day of sampling.

4.0 ANALYTICAL PROCEDURES

4.1 Sample Preparation

The samples were received in the laboratory in screw-capped glass bottles with Teflon®-lined caps, sealed with Teflon® tape and stored in coolers packed with ice. Samples were logged into the laboratory sample tracking system and stored in a secure, refrigerated (4°C) sample storage area prior to analysis. Samples were prepared for analysis within 30 days of collection and analyzed within 30 days of preparation.

All labware was washed with detergent and water and rinsed with hot tap water, rinsed with deionized water, baked at 300°C, rinsed with acetonitrile and toluene prior to use. Solvents used were HPLC grade or equivalent.

Each of the two recovered samples from each train was transferred along with rinses to separate 500 mL round bottom flasks and then evaporated to dryness under vacuum in a 65°C water bath. Each round-bottom flask was then rinsed three times with separate two (2) mL aliquots of acetonitrile (ACN) and the rinses transferred to a 10-mL volumetric flask. The sample was then brought to volume with ACN and transferred to a 15-mL vial and sealed with a Teflon®-lined lid. The vial was stored in a refrigerated sample storage area at 4°C until analysis.

4.2 Chromatographic Analyses

The procedures for the HPLC analyses of the samples are described in the following sections.

4.2.1 Standard Preparation

A 300 µg/mL stock solution of TDI piperazine urea derivative was prepared by dissolving 7.5 mg of the purified crystals of the derivatized TDI in 25 mL of

ACN. [The derivatized TDI was previously prepared by adding 1 g of the neat TDI to a solution of 1-(2-pyridyl) piperazine in ACN, evaporating to dryness and recrystallizing the urea derivative three times from ACN.] Working standards for the calibration curve were made from this stock at six concentration levels in ACN ranging from 0 to 50 $\mu\text{g/mL}$. This concentration range covered the amount of TDI expected to be collected at the host facility. This stock solution was also used to prepare the field spiking solution. A check standard was prepared from a separately prepared stock solution. This check standard fell in the middle of the calibration curve.

4.2.2 Analysis

HPLC System

The HPLC system operating parameters for analysis of standards and samples were as follows:

Instrument:	RAININ HPXL Delivery System Waters 710B WISP autosampler
Data System:	Nelson 2600 (1 volt)
Column:	Zorbax ODS (4.6 mm ID x 25 cm)
Mobile Phase:	Acetonitrile/0.1M Ammonium Acetate Buffer
Gradient:	25:75 ACN/0.1 m ammonium acetate buffer, pH 6.2, hold 2 minutes, then to 60:40 by 19.5 minutes.
Detector:	RAININ Dynamax Dual-Wavelength, Ultraviolet at 254 nm
Flow Rate:	2 mL/min
Injector Volume:	50 μL
Retention Time:	2,4-TDI, 10.2 min.; 2,6-TDI 8.5 min.

Instrument Calibration

Calibration standards were prepared at seven levels as described in Section 4.2.1. Each calibration standard was injected in duplicate. Linear regression analysis of peak area response versus concentrations of TDI was used to prepare a calibration curve. Linearity of the calibration curve was confirmed by visual inspection and verified by a correlation coefficient of 0.9995. After an initial calibration curve was obtained, the calibration check standard described in Section 4.2.1 was analyzed. This standard was injected after every 3 samples, and was used for daily calibration. This check standard consistently agreed to within 10% of the true value.

All samples were analyzed in triplicate on the HPLC. An acetonitrile blank was analyzed once per day to ensure that the system was not contaminated. A check standard was analyzed prior to sample analysis, after every 3 samples, and at the end of the sample analysis each day.

4.3 Qualitative Identification

Analytes were identified by retention time. The retention time for 2,4-TDI was 10.2 min and 8.5 min for 2,6-TDI. Figures 4-1 and 4-2 show chromatograms from the analysis of first impinger contents from QUAD run number 4 for the unspiked and spiked trains respectively. As seen in the chromatograms, the TDI peaks are well separated from the peak for unreacted 1-2 PP. The peak at 17.5 min. was not identified.

4.4 Calculations

4.4.1 Calculation of the Amount of Isocyanate Collected

A least squares linear regression analysis of the calibration data was used to calculate a correlation coefficient, slope, and intercept. Concentration was used as the independent or X-variable and response was used as the dependent or Y-variable.

Unspiked Train
Quad Run Number 4

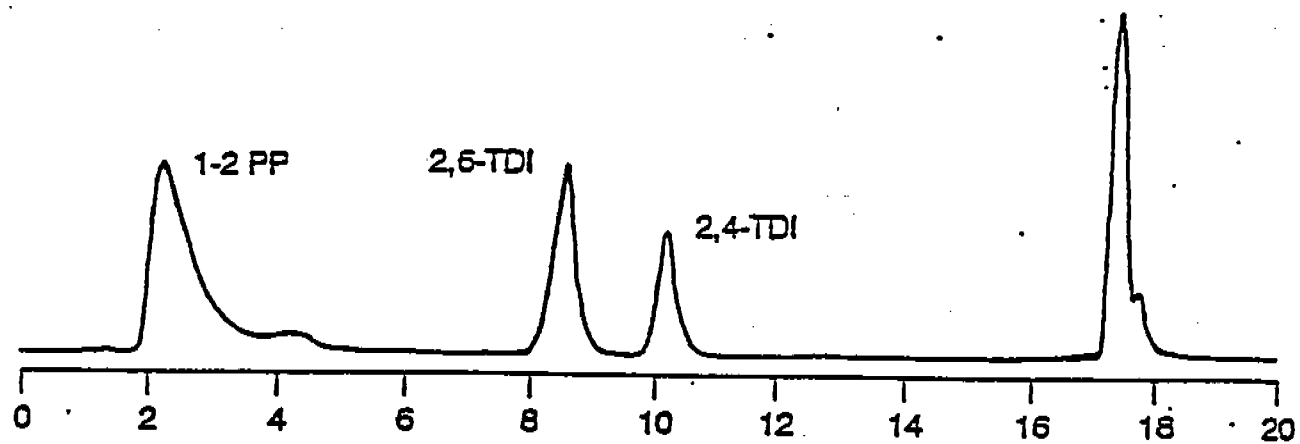


Figure 4-1. Chromatogram of Unspiked Train

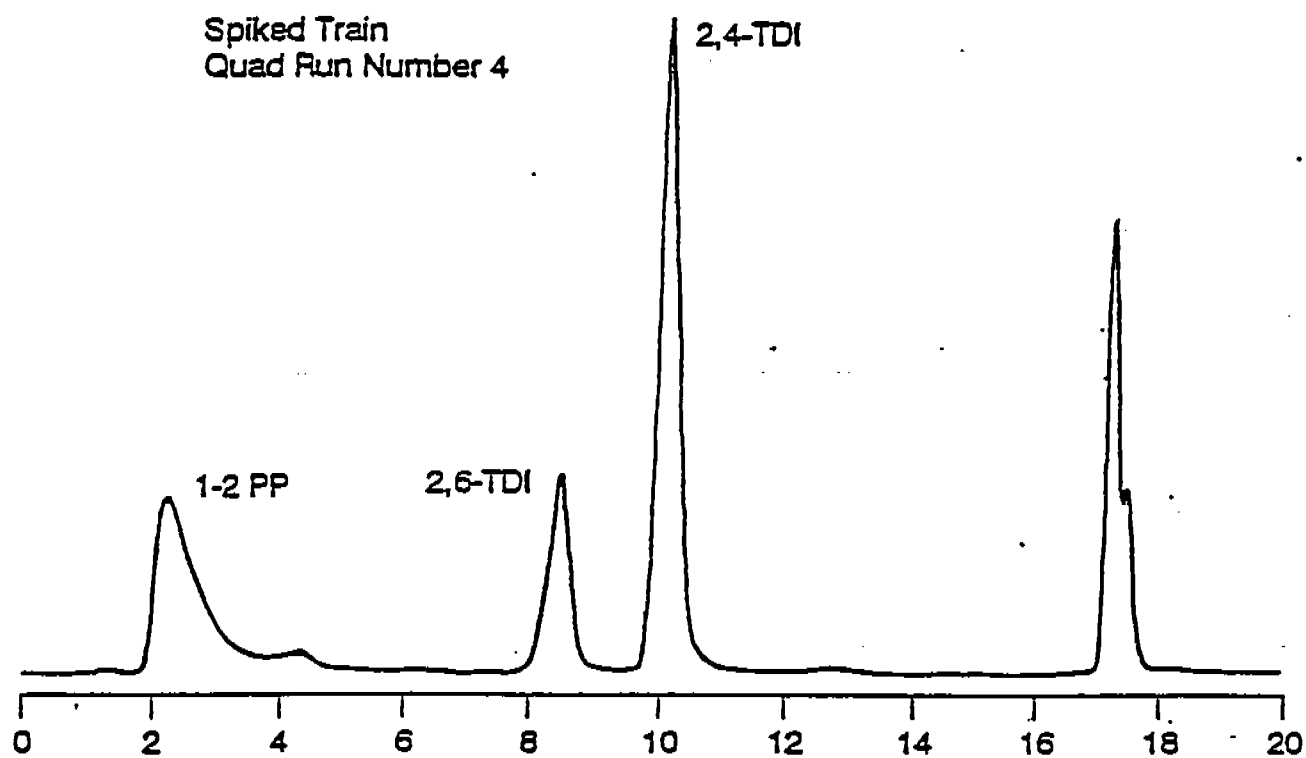


Figure 4-2. Chromatogram of Spiked Train

The concentration of isocyanate (as the derivative) in the concentrated samples was then calculated as follows:

$$\text{Concentration} = \frac{(\text{Sample Response} - \text{Intercept})}{\text{Slope}} \quad 4-1$$

The total amount (μg) collected in a sample was then calculated by multiplying the concentration ($\mu\text{g/mL}$) times the final volume (10 mL) of ACN used to redissolve the concentrated sample.

$$\text{Amount TDI derivative} = \text{Concentration } (\mu\text{g/mL}) \times \text{Final Volume (10 mL)} \quad 4-2$$

The equivalent amount of TDI required to generate this much derivative was calculated by multiplying the ratio of the molecular weights of TDI (174) and the TDI derivative (501) times the amount of TDI derivative (determined by using equation 4-2).

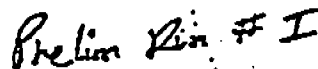
The total amount of 2,4-TDI (underivatized) collected in the unspiked and spiked trains is given in Table 4-1 and Table 4-2 respectively.

4.4.2 Normalization of the Amount of Isocyanate Collected

In order to simplify the comparison of the analytical results of the four trains in each QUAD run for subsequent calculations of bias and precision, the test plan called for the collected of 30 ft³ of sample in each train. Due to operational variabilities inherent to each train, accurate but slightly differing sample volumes resulted as shown in Table 3-3. Therefore, it was necessary to normalize the data presented in Tables 4-1 and 4-2 to a common sample volume. The sample volume to which all data were normalized was selected to be 35.31 ft³ which is equivalent to 1m³. The following stepwise calculations were used to normalize the data. The data from QUAD run number 1 are used as an example.

8-21-51 • 0-3 (MEX) •

Preliminary Data



Imaging

1233 in Total

Radon
is checked
(D)

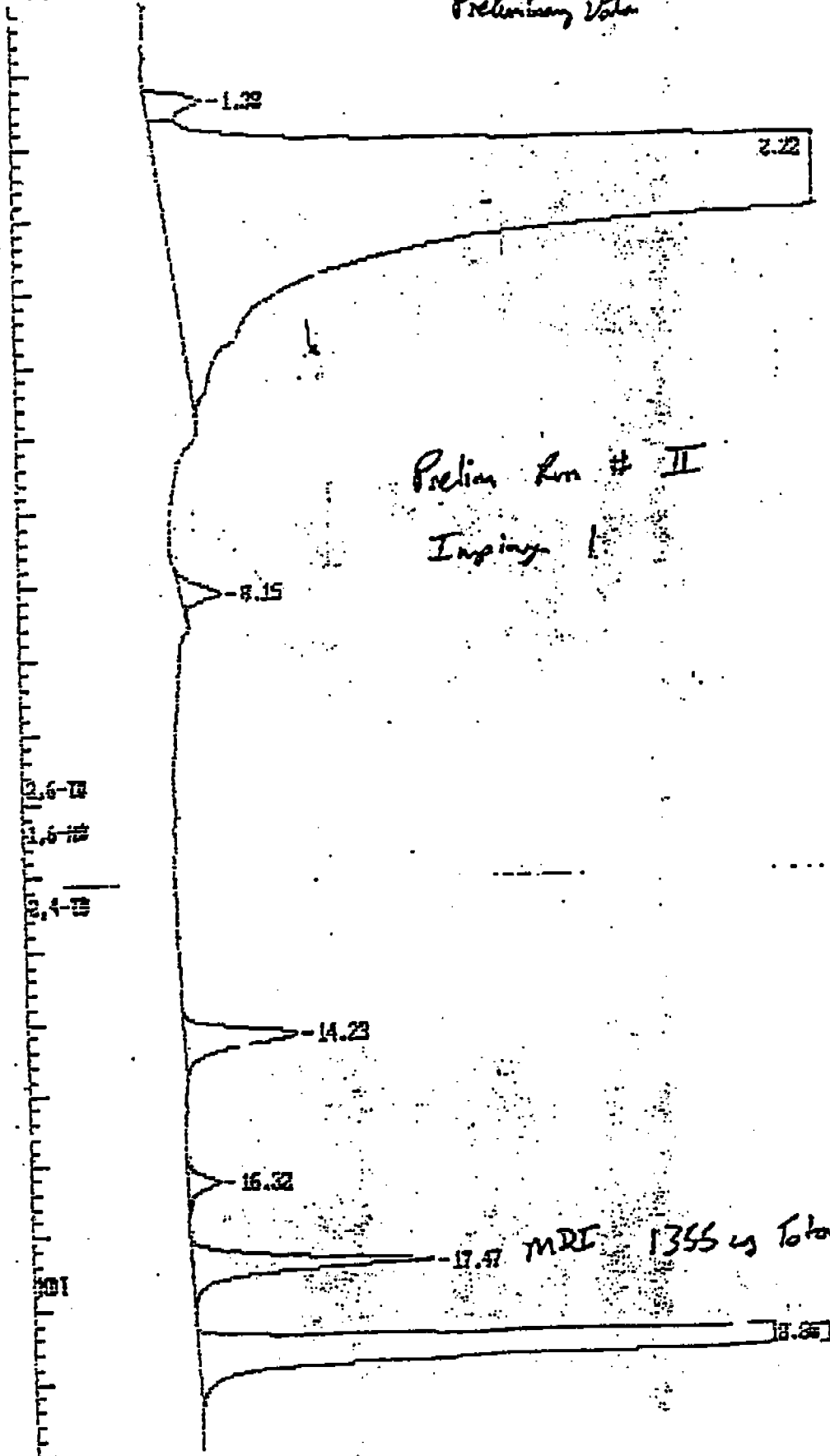
John - Police

SENT BY:

DATE: 09-10-1993

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Full Range: 50 K-Counts

Preliminary Data

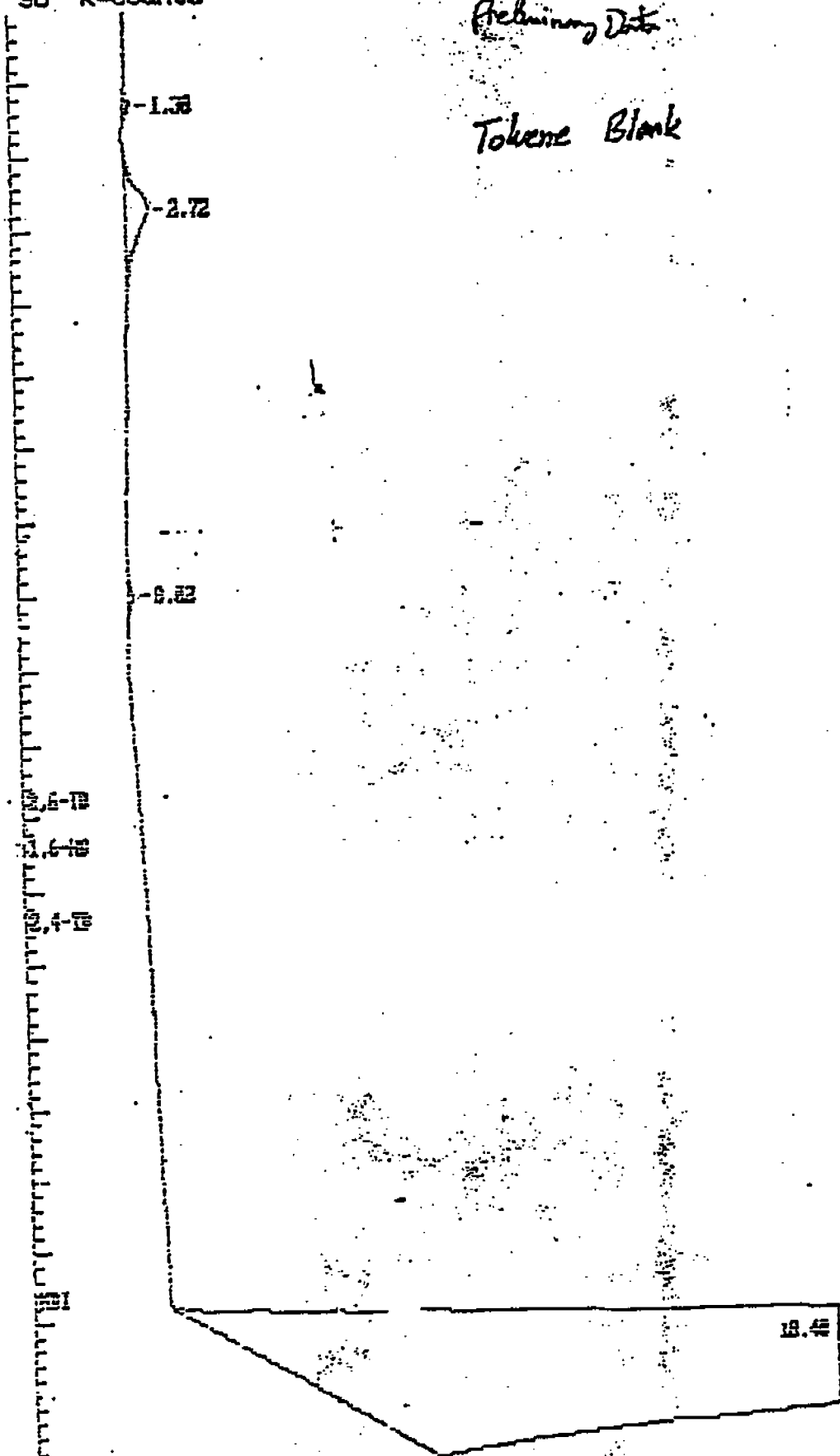


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Full Range: 50 K-Counts

0 ota

Preliminary Data

Toluene Blank



*unknown
Impurity*

SENT BY: 3-21-80 10-00 AM
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Start time: 0.00 min. Stop time: 20.00 min. Offset: 0 cts
Full Range: 50 K-Counts

Preliminary Data

Quantitative Standard
23 ug each

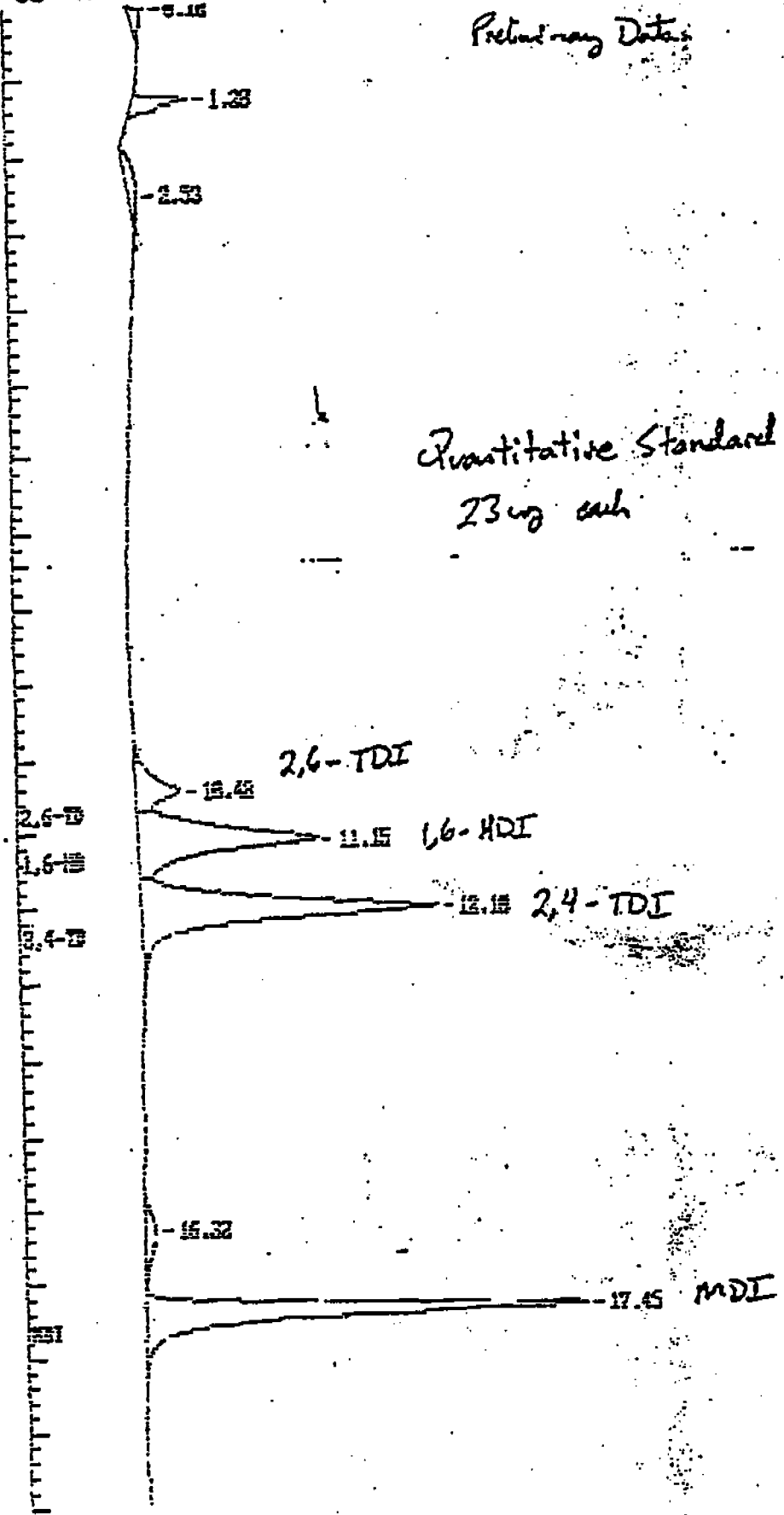


Table 4-1
2,4-TDI Detected in Unspiked Trains, µg

QUAD Run No.												
Train ¹	1			2			3			4		
	Imp 1	Imp 2	Total	Imp 1	Imp 2	Total	Imp 1	Imp 2	Total	Imp 1	Imp 2	Total
A	--	--	--	5114	61	5175	--	--	--	1832	16	1848
B	--	--	--	5224	40	5264	--	--	--	1864	24	1888
C	4409 ²	18	4427	--	--	--	3281	32	3313	--	--	--
D	4416	85	4501	--	--	--	2928	33	2960	--	--	--

¹The unspiked trains alternated from run to run, C and D then A and B.

²All values are in micrograms of underivatized TDI.

Table 4-1 (Continued)

Train ¹	QUAD Run No.										
	5			6			7			8	
	Imp 1	Imp 2	Total	Imp 1	Imp 2	Total	Imp 1	Imp 2	Total	Imp 1	Imp 2
A	--	--	--	7880	105	7993	--	--	--	3521	53
B	--	--	--	7488	89	7577	--	--	--	3805	50
C	4810	17	4827	--	--	--	2160	23	2183	--	--
D	5054	42	5096	--	--	--	2180	36	2216	--	--

¹The unspiked trains alternated from run to run, C and D then A and B.

²All values are in micrograms of underivatized TDI.

Table 4-2
2,4-TDI Detected in Spiked Trains, μg

Train ¹	QUAD Run No.											
	1			2			3			4		
	Imp 1	Imp 2	Total	Imp 1	Imp 2	Total	Imp 1	Imp 2	Total	Imp 1	Imp 2	Total
A	11943 ²	64	12007	--	--	--	11488	36	11524	--	--	--
B	11301	28	11329	--	--	--	12024	38	12062	--	--	--
C	--	--	--	12045	35	12080	--	--	--	9329	58	9387
D	--	--	--	12454	49	12503	--	--	--	9429	26	9455

¹The spiked trains alternated from run to run, A and B then C and D.

²All values are in micrograms of underivatized TDI.

Table 4-2 (Continued)

Train ¹	QUAD Run No.											
	5			6			7			8		
	Imp 1	Imp 2	Total	Imp 1	Imp 2	Total	Imp 1	Imp 2	Total	Imp 1	Imp 2	Total
A	12014	45	12059	--	--	--	10094	46	10140	--	--	--
B	12588	37	12625	--	--	--	9003	40	9043	--	--	--
C	--	--	--	15201	88	15289	--	--	--	10561	45	10606
D	--	--	--	15173	96	15269	--	--	--	10315	44	10359

¹The spiked trains alternated from run to run, A and B then C and D.

²All values are in micrograms of underivatized TDI.

- Step 1 Normalize unspiked Trains C and D first impinger amounts (μg) to the sample volume collected (cubic feet) in spiked Train A;

$$\text{Train C} \quad \frac{33.42 \text{ ft}^3}{33.02 \text{ ft}^3} \times 4409 \mu\text{g} = 4462 \mu\text{g} \quad 4-3A$$

$$\text{Train D} \quad \frac{33.42 \text{ ft}^3}{33.04 \text{ ft}^3} \times 4416 \mu\text{g} = 4467 \mu\text{g} \quad 4-3B$$

- Step 2 Average the normalized, unspiked train amounts from step 1 above. Assuming the collection efficiency of all trains to be the same, this value would also be the amount of TDI that would be collected by Train A due to sampling the stack gas;

$$\frac{4462 \mu\text{g} + 4467 \mu\text{g}}{2} = 4465 \mu\text{g} \quad 4-4$$

- Step 3 Subtract the average value (step 2) from the uncorrected amount (sampled amount plus spike) for spiked Train A, first impinger, to get recovered spike amount;

$$11943 \mu\text{g} - 4465 \mu\text{g} = 7478 \mu\text{g} \quad 4-5$$

- Step 4 Normalize the amount collected in spiked Train A, first impinger to 35.31 ft^3 using the sample volume for Train A and the value obtained in step 2;

$$\frac{35.31 \text{ ft}^3}{33.42 \text{ ft}^3} \times 4465 \mu\text{g} = 4718 \mu\text{g} \quad 4-6$$

- Step 5 Normalize the amount collected in the second impinger of spiked Train A to 35.31 ft^3 using the sample volume for Train A and the amount determined by HPLC;

$$\frac{35.31 \text{ ft}^3}{33.42 \text{ ft}^3} \times 63.9 \text{ } \mu\text{g} = 67.5 \text{ } \mu\text{g} \quad 4-7$$

Step 6 Sum the values determined from steps 3, 4 and 5 to get the total amount of TDI found in spiked Train A, normalized to 35.31 ft³;

$$7478 \text{ } \mu\text{g} + 4718 \text{ } \mu\text{g} + 67.5 \text{ } \mu\text{g} = 12264 \text{ } \mu\text{g} \quad 4-8$$

Steps 1-6 can be repeated for similar calculations for spiked Train B. The total amount of TDI collected in each of the unspiked trains can be determined by first normalizing the amounts found in the two impingers of each train to 1m³ and then summing the two values. The raw and normalized data for all analysis results are presented in Appendix A. The resulting normalized values are summarized in Tables 4-3 and 4-4.

4.5 Quality Control

Quality control procedures that were implemented for this program include:

- Adhering to applicable sampling and analysis protocols;
- Collecting and analyzing field blanks, trip blanks, reagent blanks, and laboratory blanks;
- Tracking samples from collection to analysis;
- Calibrating all analytical equipment prior to use;
- Maintaining accurate and complete written documentation;
- If any changes were made to the analytical system (i.e., column changed, column maintenance), a calibration check was performed to verify the validity of the calibration curve. If the calibration check did not meet acceptance criteria, the analytical system was recalibrated.

Table 4-3
Normalized Amount of 2,4-TDI Detected in Unspiked Trains, μg

Train ¹	QUAD Run No.							
	1	2	3	4	5	6	7	8
A	--	6287	--	2132	--	8042	--	4086
B	--	6270	--	2139	--	7608	--	4579
C	4735 ²	--	3466	--	4947	--	2557	--
D	4811	--	3166	--	5522	--	2616	--

¹The unspiked trains alternated from run to run, C and D then A and B.

²All values are in micrograms of underivatized TDI, normalized to a sample volume of 35.31 ft³ (1m³).

Table 4-4

Normalized Amount of 2,4-TDI Detected in Spiked Trains, μg

Train ¹	QUAD Run No.							
	1	2	3	4	5	6	7	8
A	12264 ²	--	11625	--	12233	--	10450	--
B	11520	--	12078	--	12717	--	9290	--
C	--	13258	--	9694	--	15471	--	11197
D	--	13733	--	9805	--	15610	--	10947

¹The spiked trains alternated from run to run, A and B then C and D.

²All values are in micrograms of underivatized TDI, normalized to a sample volume of 35.31 ft³ (1m³).

- Analysis of field spiked QC samples; and
- Analysis of check standards every 3 samples.

This section presents the results of the eight sampling runs relative to the criteria for method precision and bias. Fractional results are also presented to show the amount of isocyanate breakthrough occurring in the impinger train. All sample fractions were prepared and analyzed for toluene diisocyanate at Radian's Research Triangle Park laboratory.

5.1 Bias and Precision

Table 5-1 is a summary table which presents the results of the statistical evaluation of the test data following the EPA Method 301 criteria showing the method precision and bias for 2-4 TDI. Method 301 requires valid data from a minimum of six QUAD runs. Table 5-1 presents data from all eight runs. Precision is shown as the percent relative standard deviation of the measured amounts of TDI in the samples. Results for precision of both the spiked and unspiked samples were less than 5 percent RSD, which is well within the limits of acceptable precision (upper limit of 50%) given in EPA Method 301.

Using the data from all eight QUAD runs, method bias was measured at -395 micrograms. This value was determined to be statistically significant at the 95% confidence level, using the t statistic calculated for the analytical data. A correction factor of 1.053 was calculated for use with the method to compensate for the bias should the method be used to measure TDI emissions from similar sources.

Using the data from only seven QUAD runs (eliminating run 8 because this run had the lowest average % recovery and the final leak check for one of the trains was questionable), the method bias was -295 micrograms. This bias was not statistically significant and therefore no correction factor was calculated. In either case, the criteria for an acceptable method were met (i.e., a correction factor between 0.7 and 1.3).

Table 5-1

Summary of Method 301 Statistical Calculations

Parameter	Spiked Trains		Unspiked Trains	
	7 Runs	8 Runs	7 Runs	8 Runs
Spiked Amount ¹	7828	7828	--	--
RSD, %	3.6	3.4	4.7	5.2
Average Bias ¹	-295	-395	--	--
Bias Significant?	No	Yes	--	--
Correction Factor	1.0	1.053	--	--

¹Values are presented as μg of underivatized TDI

This section presents details of the breakthrough and recovery results for the field samples, as well as recovery information for the spiked compound (2,4-TDI).

5.2.1

Breakthrough

Tables 4-1 and 4-2 provide a summary of the combined total mass of 2,4-TDI collected in the probe/first impinger and second/third impinger samples for the unspiked and spiked trains, respectively. These totals are used as a basis for calculating breakthrough of the TDI from the first impinger to the second impinger. The mass of compound found in the probe/first impinger fraction and in the second impinger fraction were each divided by the total mass of TDI for that train and then multiplied by 100 to yield the percent of the total TDI found in the separate train sections. The results are presented in Table 5-2 and 5-3 for the spiked and unspiked trains respectively.

The average breakthrough for the spiked trains was 1.5% and for the unspiked trains 1.1%. More than 98% of the TDI was collected in the first impinger under the sampling conditions used in this study.

The amount of the toluene contained in the first impingers of each of the trains was reduced by approximately 25% (by weight) during the sampling run due to evaporation. The second impingers showed, on the average, a net gain of approximately 5%. The remainder was collected in the silica gel and the charcoal, both of which showed net weight gains. The total weight gained in the train components following the first impinger more than compensate for losses from the first impinger, probably due to the collection of a small amount of moisture. The loss of toluene from the first impinger was minimized by keeping the impingers in an ice bath and placing a water cooled condenser between the outlet of the first impinger and the inlet of the second impinger.

Table 5-2

Distribution of 2,4-TDI Within the Spiked Trains

Train ¹	Impinger No.	QUAD Run No.							
		1	2	3	4	5	6	7	8
A	1	98.5 ²	--	99.0	--	99.0	--	98.0	--
	2	1.5	--	1.0	--	1.0	--	2.0	--
B	1	99.2	--	99.1	--	99.2	--	97.0	--
	2	0.8	--	0.9	--	0.8	--	3.0	--
C	1	--	99.2	--	96.4	--	98.8	--	98.4
	2	--	0.8	--	3.6	--	1.2	--	1.6
D	1	--	99.0	--	98.5	--	98.7	--	98.4
	2	--	1.0	--	1.5	--	1.3	--	1.6
Average/ % RSD	1	98.5/0.81							
	2	1.5/54.4							

¹Spiked Trains alternate from run to run, A and B, then C and D.²Values are a percentage of the total amount of 2,4 TDI determined to be in each train.

Table 5-3

Distribution of 2,4-TDI Within the Unspiked Trains

Train ¹	Impinger No.	QUAD Run No.							
		1	2	3	4	5	6	7	8
A	1	--	98.8	--	99.1	--	98.7	--	98.5
	2	--	1.2	--	0.9	--	1.3	--	1.5
B	1	--	99.2	--	98.8	--	98.8	--	98.7
	2	--	0.8	--	1.2	--	1.2	--	1.3
C	1	99.6 ²	--	99.0	--	99.6	--	99.0	--
	2	0.4	--	1.0	--	0.4	--	1.0	--
D	1	99.1	--	98.9	--	99.2	--	98.4	--
	2	1.9	--	1.1	--	0.8	--	1.6	--
Average/ % RSD	1	98.9/0.41							
	2	1.1/37.1							

¹Unspiked Trains alternate from run to run, C and D, then A and B.²Values are a percentage of the total amount of 2,4-TDI determined to be in each train.

One of the objectives of this test program was to obtain bias and precision data to validate the proposed test method for isocyanates. Samples from two of the four trains of each quad assembly were spiked with TDI before each sampling run. The estimation of method bias is based on the percentage of the TDI spikes recovered. Analytical results used for this calculation are the averages of the triplicate analysis results for each spiked sample. A summary of the spiked TDI recovery percentages is presented in Table 5-4.

The percent recovery was calculated for each spiked train for each run following the calculation procedures outlined in steps 1-3 of Section 5.0. The value obtained at step 3, the amount of spike recovered, is divided by the actual amount of TDI spiked, 7827 μg , multiplied by 100. An average recovery was determined by averaging the 16 individual run recoveries.

The recovery for TDI ranged between 83 and 112 percent and averaged 95 percent with a %RSD of 8.2.

5.3

Quality Assurance/Quality Control

As a part of the testing for Work Assignment No. 55, Radian designed and implemented a quality assurance/quality control (QA/QC) effort tailored to meet the specific needs of this project. The testing was conducted in accordance with QA/QC procedures described in the Quality Assurance Project Plan (QAPP). The results of the QA/QC effort demonstrate that the data are reliable and meet project objectives for completeness and representativeness. The data met the QA objectives for precision and accuracy and there are no data quality issues that effect conclusions regarding the objectives of this project.

Table 5-4

Percent Recovery of the Spiked 2,4-TDI

Train ¹	QUAD Run No.							
	1	2	3	4	5	6	7	8
A	96 ²	--	106	--	89	--	100	--
B	86	--	112	--	96	--	86	--
C	--	89	--	97	--	98	--	88
D	--	95	--	98	--	99	--	83
Average	95							
% RSD	8.2							

¹Spiked Trains alternated from run to run, A and B, then C and D.²Values are a percentage based upon a spiked amount of 7827.8 µg as 2,4-TDI.

The primary objectives of the QA/QC effort were to control, assess, and document data quality. In order to accomplish these objectives, the QA/QC approach consisted of the following key elements:

- Definition of data quality objectives that reflect the overall technical objectives of the project;
- Design of a sampling, analytical, QA/QC, and data analysis system to meet these objectives; and
- Initiation of corrective action when measurement system performance did not meet the specifications.

These elements include the use of selected standard sampling and analytical procedures as components of the overall approach in addition to, specified calibration requirements, QC checks, data reduction and validation procedures, and sample tracking.

A summary of analysis results for QA/QC samples, which includes measures of precision and accuracy and limitations in the use of these data is presented in this section.

5.3.1 Overview of Data Quality

The QAPjP established specific QA objectives for precision (15% RSD), accuracy ($\pm 30\%$), and completeness (100%) for the determination of TDI emissions. The statistical results presented in Table 5-1 and the % recovery values given in Table 5-4 show that the objectives were met. The data quality acceptance criteria and the experimental results are summarized in Table 5-5. Results for spike/spike duplicates and triplicate analyses were compared with the criteria. In all cases the criteria were met. Other data quality indicators for each type of analysis are also presented throughout the remainder of Section 5.3.

There are no cases where data quality issues impair the study's conclusions with respect to the validity of the sampling and analytical test method procedures. With

Table 5-5**Data Quality Acceptance Criteria and Results**

Parameter	Criteria	Results
TDI Spike Recovery	70 - 130%	83 - 112%
TDI Analysis Results QUAD Train, % RSD	15%	5%
Individual DGM Correction Factor Agreement	$\pm 2\%$ of Avg	$< 2\%$
Analytical Balance	≤ 0.1 g of Class S Weights	< 0.1 g
HPLC Linearity Correlation Coeff.	> 0.995	0.9995
HPLC Retention Time Variation	$\pm 15\%$	$\pm 10\%$
HPLC Calibration Check	$\pm 10\%$ of Curve	$\pm 9\%$
HPLC System Blank	$< 0.1\%$ Analyte level	$< 0.1\%$
HPLC Replicate Analyses	$\pm 10\%$ of 1st injection	$\pm 2\%$
HPLC Method Spikes	$\pm 20\%$ of theoretical	$\pm 5\%$

exception of a limited number of samples, the quality of measurement data generated for the test parameters fully meets the data quality objectives outlined in the QAPjP.

5.3.2 Sampling Quality Control

Quality control activities associated with the field sampling are described in the QAPjP. These activities include adherence to accepted reference method protocols, use of standardized data recording sheets, equipment calibration, and collection of field blanks.

Stack sampling QC data, including sampling rates, sample volume collected, maximum recorded leak rate, and maximum allowable leak rate, are summarized in Table 5-6 for each run. All of the data quality indicators are within acceptable limits, with the exception of a slightly high leak rate value for Train C Run 8. However, this train was leak checked at a vacuum of 7 inches of mercury which was almost twice that achieved during sampling and the leak would therefore have very little, if any, effect on the data. The leak rate criterion is $<4\%$ of the average sampling rate or 0.02 dscf, whichever is less.

5.3.3 Sample Storage and Holding Time

Sample hold times specified in the QAPP were met for all samples. All samples were prepared within 30 days of collection and analyzed within 30 days of preparation.

5.3.4 Analytical Quality Control

Results for method spikes, field spikes, field blanks, reagent blanks and method blanks are summarized in Table 5-7. These samples served the dual purpose of controlling and assessing measurement data quality, and providing the basis for precision and accuracy estimates. The QC acceptance criteria for each of these types of samples

Table 5-6
Sampling Train Leak Summary

Rm Number	Std. Metered Volume (dscf)	Average Sampling Rate (dscfm)	Maximum Leak Check (dscf @ in Hg)	4% Sample Rate (dscfm)	Acceptable ^a Leak Rate?
1A	33.42	0.743	0.010 @ 10	0.030	Yes
1B	33.89	0.753	0.010 @ 15	0.030	Yes
1C	33.02	0.734	0.010 @ 8	0.029	Yes
1D	33.04	0.734	0.020 @ 10	0.029	Yes
2A	29.07	0.727	0.016 @ 8	0.029	Yes
2B	29.65	0.741	0.009 @ 8	0.030	Yes
2C	28.67	0.717	0.010 @ 7	0.029	Yes
2D	28.40	0.710	0.010 @ 8	0.028	Yes
3A	34.24	0.571	0.012 @ 10	0.023	Yes
3B	35.15	0.586	0.010 @ 8	0.023	Yes
3C	33.75	0.563	0.009 @ 8	0.023	Yes
3D	33.01	0.550	0.020 @ 5	0.022	Yes
4A	30.60	0.765	0.012 @ 8	0.031	Yes
4B	31.17	0.779	0.012 @ 7	0.031	Yes
4C	30.35	0.759	0.008 @ 7	0.030	Yes
4D	29.54	0.739	0.015 @ 10	0.030	Yes
5A	34.14	0.569	0.014 @ 10	0.023	Yes
5B	34.70	0.578	0.012 @ 8	0.023	Yes
5C	34.46	0.574	0.012 @ 8	0.023	Yes
5D	32.59	0.543	0.016 @ 7	0.022	Yes
6A	35.10	0.780	0.007 @ 7	0.031	Yes
6B	35.17	0.782	0.010 @ 8	0.031	Yes
6C	34.49	0.766	0.008 @ 7	0.031	Yes
6D	33.78	0.751	0.008 @ 10	0.030	Yes
7A	31.11	0.778	0.015 @ 9	0.031	Yes
7B	31.94	0.799	0.011 @ 8	0.032	Yes
7C	30.14	0.754	0.009 @ 7	0.030	Yes
7D	29.91	0.748	0.014 @ 10	0.030	Yes
8A	30.89	0.772	0.009 @ 10	0.031	Yes
8B	29.73	0.743	0.011 @ 8	0.030	Yes
8C	30.49	0.762	0.021 @ 7	0.030	No
8D	31.95	0.799	0.018 @ 8	0.032	Yes

^aThe maximum acceptable leak rate is the lesser of 0.020 dscfm or 4% of the average sampling rate.

Table 5-7

Summary of Analytical Quality Control Results

Sample ID	Total Detected μg	Theoretical μg	Percent Error %
Field Blank A	2.5	NA ⁴	NA
Field Blank B	8.3	NA	NA
Field Blank C	6.4	NA	NA
Field Spike 1	7570	7828	96.7
Field Spike 2	7686	7828	98.2
Method Spike 1	8120	7828	104
Method Spike 2	7838	7828	100
Method Spike 3	7890	7828	101
Method Spike 4	7945	7828	101
Toluene Reagent Blank ¹	0.5	NA	NA
ACN Reagent Blank ²	0.4	NA	NA
Method Blank ³	10.2	NA	NA

¹Average of four, ranging from 0.1 to 1.2 μg

²Average of four, ranging from 0.1 to 0.8 μg

³Average of three, ranging from 0.3 to 20.7 μg

⁴NA, Not Applicable

were met as shown in Table 5-5. Field blanks were collected by assembling a sampling train as if to collect a sample, transporting to the sampling location, leak checking and returning the train to the onsite laboratory for recovery. Field spikes and method spikes were prepared by spiking approximately 300 mL of the toluene 1,2-PP solution with 15 mL of the field spiking solution. Method and reagent blanks were prepared by evaporating approximately 300 mL of solvent to dryness and dissolving any residue with 10 mL of ACN. All spikes and blanks met the data acceptance criteria listed in Table 5-5.

No blank contamination problems were identified during the analysis of field and laboratory blanks and no blank corrections were performed for the reported data. All blank analysis data are presented along with other QC and field sample results in Appendix A.

APPENDIX A

Analytical Data for Samples, Blanks, Spikes and Quality Control Samples

Sample Name	AREA	AMOUNT ug/mL	QC Con ug/mL	QC Bias %	Dilution Factor	Amount Sample ug	Avg Amt Sample ug	Volume Sampled Cu Ft	Sampling Factor	Adjusted Avg ug	Total Train ug	Amount Spiked ug	Spike Recovery %	Train ID
ISO-SCF-32293-4	1263013	5.90	5.40641	9%	2000	11931.6	11942.9	33.42	1.05669	12196.0	12263.5	7827.81	95.69%	I-A-1
ISO-SCF-32293-4	1251783	5.86	5.40641	8%	2000	11930.1								
ISO-SCF-32293-4	1249199	5.84	5.40641	8%	2000	11966.8								
ARL-1	1277072	5.97			1000	64.1	63.9	33.42	1.05669	67.5				I-A-2
ARL-1	1276918	5.97			1000	64.4								
ARL-1	1280852	5.98			1000	63.1								
ARL-2	135291	0.64			2000	11178.7	11300.8	33.89	1.04204	11491.1	11520.1	7827.81	86.19%	I-B-1
ARL-2	135913	0.64			2000	11148.3								
ARL-2	131152	0.63			2000	11175.1								
ARL-3	1196354	5.59			1000	28.6	27.8	33.89	1.04204	29.0				I-B-2
ARL-3	1214532	5.67			1000	27.7								
ARL-3	1217429	5.69			1000	27.2								
ARL-4	59159	0.29			2000									
ARL-4	57134	0.28			2000									
ARL-4	56201	0.27			2000									
ISO-SCF-32293-4	1255771	5.87	5.40641	9%	2000	4418.4	4409.3	33.02	1.06949	4715.7	4735.0			I-C-1
ISO-SCF-32293-4	1251918	5.85	5.40641	8%	2000	4411.3								
ISO-SCF-32293-4	1242330	5.80	5.40641	7%	2000	4398.2								
ARL-5	471546	2.21			1000	17.8	18.1	33.02	1.06949	19.3				I-C-2
ARL-5	470785	2.21			1000	18.3								
ARL-5	469380	2.20			1000	18.2								
ARL-6	35898	0.18			2000	4399.5	4416.1	33.04	1.06885	4720.1	4811.1			I-D-1
ARL-6	37029	0.18			2000	4324.4								
ARL-6	36906	0.18			2000	4524.4								
ARL-7	469526	2.20			1000	85.0	85.1	33.04	1.06885	90.9				I-D-2
ARL-7	461467	2.16			1000	84.8								
ARL-7	482909	2.26			1000	85.4								
ARL-8	180144	0.85			1000									
ARL-8	179633	0.85			1000									
ARL-8	181047	0.85			1000									
ISO-SCF-32293-4	1238919	5.79	5.40641	7%										
ISO-SCF-32293-4	1245039	5.82	5.40641	8%										
ISO-SCF-32293-4	1235673	5.77	5.40641	7%										

Sample Name	AREA	AMOUNT ug/mL	QC Con ug/mL	QC Bias %	Dilution Factor	Amount Sample ug	Avg Amt Sample ug	Volume Sampled Cu Ft	Sampling Factor	Adjusted Avg ug	Total Train ug	Amount Spiked ug	Spike Recovery %	Train ID
ARL-9	544346	2.55			2000	5097.4	5114.2	29.07	1.21481	6212.9	6287.4			2-A-1
ARL-9	548157	2.57			2000	5112.9								
ARL-9	545954	2.56			2000	5112.4								
ARL-10	130306	0.62			100	61.8	61.4	29.07	1.21481	74.6				2-A-2
ARL-10	130940	0.62			100	62.1								
ARL-10	127140	0.60			100	60.3								
ARL-10	127140	0.60			2000	5114.9	5224.4	29.65	1.19105	6222.5	6269.9			2-B-1
ARL-11	567669	2.66			2000	5275.7								
ARL-11	563460	2.64			2000	5082.6								
ARL-11	542754	2.54			2000	39.9	39.8	29.65	1.19105	47.4				2-B-2
ARL-12	83414	0.40			100	40.0								
ARL-12	83620	0.40			100	39.4								
ARL-12	82237	0.39			100	5.7								
ISO-SCF-32293-4	1220899	5.70	5.40641	6%	1	5.7								
ISO-SCF-32293-4	1232005	5.76	5.40641	6%	1	5.8								
ISO-SCF-32293-4	1230936	5.75	5.40641	6%	1	5.8								
ARL-13	1287864	6.02			2000	12032.2	12015.3	28.67	1.23176	13215.1	13258.2	7827.81	89.16%	2-C-1
ARL-13	1288870	6.02			2000	12041.6								
ARL-13	1291013	6.03			2000	12061.9								
ARL-14	71522	0.34			100	34.4	35.0	28.67	1.23176	43.1				2-C-2
ARL-14	73423	0.35			100	35.3								
ARL-14	73513	0.35			100	35.3								
ARL-15	1335291	6.24			2000	12474.6	12454.1	28.40	1.24347	13671.5	13732.6	7827.81	95.22%	2-D-1
ARL-15	1334709	6.23			2000	12469.2								
ARL-15	1329284	6.21			2000	12418.6								
ARL-16	103190	0.49			100	49.1	49.1	28.40	1.24347	61.1				2-D-2
ARL-16	103848	0.49			100	49.1								
ARL-16	102349	0.49			100	48.7								
ISO-SCF-32293-4	1236426	5.82	5.40641	8%	1	5.8								
ISO-SCF-32293-4	1237852	5.78	5.40641	7%	1	5.8								
ISO-SCF-32293-4	1239959	5.79	5.40641	7%	1	5.8								

Sample Name	AREA	AMOUNT ug/mL	QC Con ug/mL	QC Bias %	Dilution Factor	Amount Sample ug	Avg Amt Sample ug	Volume Sampled Cu Ft	Sampling Factor	Adjusted Avg ug	Total Train ug	Amount Spiked ug	Spike Recovery %	Train ID
ARL-17	1229990	5.75			2000	11492.4	11487.9	34.24	1.03139	11587.8	11624.8	7827.81	106.14%	3-A-1
ARL-17	1214060	5.67			2000	11343.9								
ARL-17	1244450	5.81			2000	11627.1								
ARL-18	75825	0.36			100	36.4	35.9	34.24	1.03139	37.0				3-A-2
ARL-18	74917	0.36			100	36.0								
ARL-18	73672	0.35			100	35.4								
ARL-19	1282836	5.99			2000	11985.1	12024.4	35.15	1.00468	12039.7	12077.7	7827.81	111.93%	3-B-1
ARL-19	1289518	6.02			2000	12047.7								
ARL-19	1288725	6.02			2000	12040.3								
ARL-20	79007	0.38			100	37.9	37.8	35.15	1.00468	38.0				3-B-2
ARL-20	78713	0.38			100	37.7								
ARL-20	79021	0.38			100	37.9								
ISO-SCF-32293-4	1263449	5.90	5.40641	9%	1	5.9								
ISO-SCF-32293-4	1253499	5.86	5.40641	8%	1	5.9								
ISO-SCF-32293-4	1260480	5.89	5.40641	9%	1	5.9								
ARL-21	351376	1.65			2000	3297.6	3281.0	33.75	1.04636	3433.1	3466.4			3-C-1
ARL-21	343323	1.61			2000	3222.4								
ARL-21	354099	1.66			2000	3321.0								
ARL-22	65492	0.32			100	31.6	31.8	33.75	1.04636	33.3				3-C-2
ARL-22	66002	0.32			100	31.8								
ARL-22	66603	0.32			100	32.1								
ARL-23	319713	1.50			2000	3002.2	2927.6	33.01	1.06982	3132.0	3165.7			3-D-1
ARL-23	310818	1.46			2000	2919.3								
ARL-23	304609	1.43			2000	2861.4								
ARL-24	65115	0.31			100	31.4	31.5	33.01	1.06982	33.7				3-D-2
ARL-24	66054	0.32			100	31.8								
ARL-24	64767	0.31			100	31.2								
ISO-SCF-32293-4	1223529	5.72	5.40641	6%	1	5.7								
ISO-SCF-32293-4	1220297	5.70	5.40641	5%	1	5.7								
ISO-SCF-32293-4	1163133	5.70	5.40641	5%										

Sample Name	AREA	AMOUNT ug/mL	QC Con ug/mL	QC Bias %	Dilution Factor	Amount Sample ug	Avg Amt Sample ug	Volume Sampled Cu ft	Sampling Factor	Adjusted Avg ug	Total Train ug	Amount Spiked ug	Spike Recovery %	Train ID
ARL-25	198810	0.94			2000	1874.6	1831.7	30.60	1.15407	2113.9	2132.1			4-A-1
ARL-25	195931	0.92			2000	1847.7								
ARL-25	187888	0.89			2000	1772.7								
ARL-26	31316	0.17			100	16.6	15.8	30.60	1.15407	18.3				4-A-2
ARL-26	32875	0.16			100	16.3								
ARL-26	29079	0.15			100	14.6								
ARL-27	200805	0.93			2000	1893.2	1864.2	31.17	1.13297	2112.1	2138.7			4-B-1
ARL-27	200538	0.95			2000	1890.7								
ARL-27	191787	0.90			2000	1808.9								
ARL-28	48281	0.24			100	21.5	23.5	31.17	1.13297	26.6				4-B-2
ARL-28	49506	0.24			100	24.1								
ARL-28	46705	0.23			100	22.8								
ISO-SCF-32293-4	1202635	5.62	5.40641	4%	1	5.6								
ISO-SCF-32293-4	1219147	5.70	5.40641	5%	1	5.7								
ARL-29	1001159	4.68			2000	9358.1	9129.4	30.35	1.16358	9626.4	9693.9	7827.81	96.56%	4-C-1
ARL-29	987039	4.61			2000	9226.4								
ARL-29	1006035	4.70			2000	9403.6								
ARL-30	124507	0.59			100	59.1	58.0	30.35	1.16358	67.5				4-C-2
ARL-30	122754	0.58			100	58.3								
ARL-30	110182	0.57			100	56.6								
ARL-31	1004933	4.70			2000	9393.3	9428.7	29.54	1.19549	9774.2	9804.7	7827.81	97.97%	4-D-1
ARL-31	1018359	4.76			2000	9518.5								
ARL-31	1002870	4.69			2000	9374.1								
ARL-32	53598	0.26			100	26.0	25.5	29.54	1.19549	30.5				4-D-2
ARL-32	53113	0.26			100	25.8								
ARL-32	50832	0.25			100	24.7								
ISO-SCF-32293-4	1200453	5.61	5.40641	4%	1	5.6								
ISO-SCF-32293-4	1204115	5.63	5.40641	4%	1	5.6								
ISO-SCF-32293-4	1189454	5.56	5.40641	3%	1	5.6								

Sample Name	AREA	AMOUNT ug/mL	QC Con ug/mL	QC Bias %	Dilution Factor	Amount Sample ug	Avg Amt Sample ug	Volume Sampled Cu Fi	Sampling Factor	Adjusted Avg ug	Total Train ug	Amount Spiked ug	Spike Recovery %	Train ID
ARL-33	1109769	6.12			2000	12236.3	12014.2	34.14	1.03441	12187.3	12233.3	7827.81	89.41%	5-A-1
ARL-33	1323802	6.18			2000	12367.4								
ARL-33	1224220	5.72			2000	11438.7								
ARL-34	101486	0.49			100	49.3	44.5	34.14	1.03441	46.1				5-B-1
ARL-34	101836	0.49			100	49.4								
ARL-34	72585	0.35			100	34.9								
ARL-35	1369996	6.40			2000	12798.3	12588.1	34.70	1.01771	12678.6	12716.7	7827.81	95.59%	5-B-1
ARL-35	1382908	6.46			2000	12918.7								
ARL-35	1289467	6.02			2000	12047.2								
ARL-36	84360	0.40			100	40.4	37.4	34.70	1.01771	38.0				5-B-2
ARL-36	85164	0.41			100	40.7								
ARL-38	64482	0.31			100	31.1								
ISO-SCF-32293-4	1198549	5.60	5.40641	4%	1	5.6								
ISO-SCF-32293-4	1178529	5.31	5.40641	2%	1	5.5								
ARL-37	511915	2.40			2000	4794.9	4809.8	34.46	1.02480	4929.1	4946.9			5-C-1
ARL-37	520867	2.44			2000	4876.5								
ARL-37	507945	2.38			2000	4757.9								
ARL-38	36452	0.18			100	18.0	17.4	34.46	1.02480	17.8				5-C-2
ARL-38	36482	0.18			100	18.0								
ARL-38	32321	0.16			100	16.1								
ARL-39	532851	2.50			2000	4990.2	5054.0	32.59	1.08360	5476.5	5521.9			5-D-1
ARL-39	544154	2.55			2000	5095.6								
ARL-39	542068	2.54			2000	5076.1								
ARL-40	80692	0.43			100	43.3	41.9	32.59	1.08360	45.4				5-D-2
ARL-40	82975	0.40			100	39.7								
ARL-40	88246	0.43			100	42.6								
ISO-SCF-32293-4	1187611	5.55	5.40641	3%	1	5.5								
ISO-SCF-32293-4	1199484	5.60	5.40641	4%	1	5.6								
ISO-SCF-32293-4	1183133	5.53	5.40641	2%	1	5.5								

Sample Name	AREA	AMOUNT ug/mL	QC Con ug/mL	QC Bias %	Dilution Factor	Amount Sample ug	Avg Amt Sample ug	Volume Sampled Cu Fl	Sampling Factor	Adjusted Avg ug	Total Train ug	Amount Spiked ug	Spike Recovery %	Train ID
ARL-41	861252	4.03			2000	8051.2	7887.9	35.10	1.00612	7936.1	8041.6			6-A-1
ARL-41	860232	4.02			2000	8043.7								
ARL-41	809094	3.78			2000	7566.7								
ARL-42	227095	1.07			100	106.9	104.8	35.10	1.00612	105.4				6-A-2
ARL-42	228142	1.07			100	107.4								
ARL-42	212430	1.00			100	100.1								
ARL-43	815730	3.81			2000	7628.6	7488.0	35.17	1.00411	7518.8	7607.6			6-B-1
ARL-43	825689	3.86			2000	7721.5								
ARL-43	760533	3.56			2000	7113.8								
ARL-44	193894	0.91			100	91.4	88.5	35.17	1.00411	88.8				6-B-2
ARL-44	197908	0.93			100	93.3								
ARL-44	170746	0.81			100	80.6								
ISO-SCF-32293-4	1189088	5.56	5.40641	3%	1	5.6								
ISO-SCF-32293-4	1190921	5.56	5.40641	3%	1	5.6								
ARL-45	1656820	7.74			2000	15473.5	15201.1	34.49	1.02391	15381.5	15471.2	7827.81	97.69%	6-C-1
ARL-45	1652121	7.71			2000	15429.7								
ARL-45	1573883	7.35			2000	14780.0								
ARL-46	187832	0.89			100	88.6	87.6	34.49	1.02391	89.7				6-C-2
ARL-46	195647	0.92			100	92.3								
ARL-46	173379	0.82			100	81.9								
ARL-47	1649873	7.70			2000	15408.7	15173.2	33.78	1.04543	15509.0	15609.8	7827.81	99.46%	6-D-1
ARL-47	1634325	7.63			2000	15263.7								
ARL-47	1588678	7.42			2000	14847.3								
ARL-48	220417	1.04			100	103.8	96.3	33.78	1.04543	100.7				6-D-2
ARL-48	206802	0.97			100	97.5								
ARL-48	186023	0.88			100	87.8								
ISO-SCF-32293-4	1205054	5.63	5.40641	4%	1	5.6								
ISO-SCF-32293-4	1195876	5.59	5.40641	3%	1	5.6								
ISO-SCF-32293-4	1183664	5.53	5.40641	2%	1	5.5								

Sample Name	AREA	AMOUNT ug/mL	QC Con ug/mL	QC Bias %	Dilution Factor	Amount Sample ug	Avg Amt Sample ug	Volume Sampled Cu/Pt	Sampling Factor	Adjusted Avg ug	Total Train ug	Amount Spiked ug	Spike Recovery %	Train ID
ARL-49	1081312	5.05			2000	10105.7	10094.4	31.11	1.13515	10398.3	10450.0	7827.81	100.45%	7-A-1
ARL-49	1074952	5.02			2000	10016.4								
ARL-49	1084020	5.07			2000	10131.0								
ARL-50	98427	0.47			100	46.9	45.6	31.11	1.13515	51.8				7-A-2
ARL-50	96270	0.46			100	45.9								
ARL-50	92145	0.44			100	44.0								
ARL-51	963252	4.30			2000	9004.6	9002.6	31.94	1.10566	9246.5	9290.2	7827.81	85.63%	7-B-1
ARL-51	970463	4.54			2000	9071.8								
ARL-51	955412	4.47			2000	8931.4								
ARL-52	83965	0.40			100	40.2	39.5	31.94	1.10566	43.6				7-B-2
ARL-52	83998	0.40			100	40.2								
ARL-52	79455	0.38			100	38.1								
ISO-SCF-32293-4	1194001	5.58	5.40641	3%	1	5.6								
ISO-SCF-32293-4	1201282	5.61	5.40641	4%	1	5.6								
ARL-53	230346	1.08			2000	2168.7	2159.8	30.14	1.17169	2530.6	2557.9			7-C-1
ARL-53	232911	1.10			2000	2192.6								
ARL-53	224911	1.06			2000	2118.0								
ARL-54	49290	0.24			100	24.0	23.3	30.14	1.17169	27.3				7-C-2
ARL-54	49749	0.24			100	24.2								
ARL-54	44499	0.22			100	21.8								
ARL-55	237247	1.12			2000	2233.1	2180.2	29.91	1.18070	2574.2	2616.4			7-D-1
ARL-55	228829	1.08			2000	2151.5								
ARL-55	226680	1.08			2000	2153.0								
ARL-56	75486	0.36			100	36.2	35.8	29.91	1.18070	42.3				7-D-2
ARL-56	75034	0.36			100	36.0								
ARL-58	73273	0.35			100	35.2								
ISO-SCF-32293-4	1201622	5.61	5.40641	4%	1	5.6								
ISO-SCF-32293-4	1192039	5.57	5.40641	3%	1	5.6								
ISO-SCF-32293-4	1184281	5.53	5.40641	2%	1	5.5								

Sample Name	AREA	AMOUNT ug/mL	QC Con ug/mL	QC Bias %	Dilution Factor	Amount Sample ug	Avg Amt Sample ug	Volume Sampled Cu Ft	Sampling Factor	Adjusted Avg ug	Total Train ug	Amount Spiked ug	Spike Recovery %	Train ID
ARL-57	374801	1.76			2000	3516.0	3520.7	30.89	1.14324	4025.0	4086.0			8-A-1
ARL-57	377410	1.77			2000	3540.4								
ARL-57	373681	1.75			2000	3505.6								
ARL-58	111353	0.51			100	52.9	53.4	30.89	1.14324	61.0				8-A-2
ARL-58	112493	0.51			100	53.5								
ARL-58	113066	0.54			100	53.7								
ARL-58	406883	1.91			2000	3815.3	3805.4	29.71	1.18785	4520.2	4579.2			8-B-1
ARL-59	401924	1.88			2000	3769.0								
ARL-59	408657	1.92			2000	3811.8	49.7	29.71	1.18785	59.0				8-B-2
ARL-60	105005	0.50			100	50.0								
ARL-60	104950	0.50			100	50.0								
ARL-60	102971	0.49			100	49.0								
ISO-SCF-32293-4	1197542	5.59	5.40641	3%	1	5.6								
ISO-SCF-32293-4	1200088	5.61	5.40641	4%	1	5.6								
ISO-SCF-32293-4	1190471	5.56	5.40641	3%	1	5.6								
ARL-61	1137017	5.31			2000	10625.3	10561.2	30.49	1.15824	11144.9	11197.4	7827.81	88.46%	8-C-1
ARL-61	1120589	5.24			2000	10471.9								
ARL-61	1132853	5.29			2000	10586.4								
ARL-62	94047	0.45			100	45.2	45.3	30.49	1.15824	52.5				8-C-2
ARL-62	95991	0.46			100	45.8								
ARL-62	94335	0.45			100	45.0								
ARL-63	1108755	5.18			2000	10361.7	10314.5	31.95	1.10531	10721.6	10770.2	7827.81	83.01%	8-D-1
ARL-63	1096270	5.12			2000	10245.2								
ARL-63	1106072	5.17			2000	10336.7								
ARL-64	92259	0.44			100	44.0	44.0	31.95	1.10531	48.6				8-D-2
ARL-64	92558	0.44			100	44.2								
ARL-64	91687	0.44			100	43.8								
ISO-SCF-32293-4	1186551	5.54	5.40641	3%	1	5.5								
ISO-SCF-32293-4	1187157	5.55	5.40641	3%	1	5.5								
ISO-SCF-32293-4	1196473	5.59	5.40641	3%	1	5.6								

Sample Name	FILE	AREA	AMOUNT ug/mL	QC Con ug/mL	QC Bias %	Dilution Factor	Amount Sample	Avg Amt Sample	Amount Spiked	Spike Recovery	Train ID
ISO-SCF-32293-4	S3083F4	1263013	5.90	5.41	9%	1	5.9	5.9			QC
ISO-SCF-32293-4	S3083F5	1253783	5.86	5.41	8%	1	5.9				
ISO-SCF-32293-4	S3083F6	1249199	5.84	5.41	8%	1	5.8				FBA
ARL-81	S3083F19	30452	0.15			10	1.5	1.6			
ARL-81	S3083F20	31446	0.16			10	1.6				
ARL-81	S3083F21	33323	0.17			10	1.7				
ARL-104	S3083F22	809699	3.79			2000	7572.4	7569.9	7827.81	97%	FS-1
ARL-104	S3083F23	808639	3.78			2000	7562.7				
ARL-104	S3083F24	809932	3.79			2000	7574.7				QC
ISO-SCF-32293-4	S3083F25	1255771	5.87	5.41	9%	1	5.9	5.8			
ISO-SCF-32293-4	S3083F26	1231918	5.85	5.41	8%	1	5.8				
ISO-SCF-32293-4	S3083F27	1242310	5.80	5.41	7%	1	5.8				FBA
ARL-82	S3083F40	16055	0.08			10	0.8	0.9			
ARL-82	S3083F41	16597	0.09			10	0.9				
ARL-82	S3083F42	16113	0.09			10	0.9				
ARL-105	S3083F43	832058	3.89			2000	7780.9	7686.3	7827.81	98%	FS-2
ARL-105	S3083F44	822507	3.85			2000	7691.8				
ARL-105	S3083F45	811167	3.79			2000	7386.1				QC
ISO-SCF-32293-4	S3083F46	1238919	5.79	5.41	7%	1	5.8	5.8			
ISO-SCF-32293-4	S3083F47	1245039	5.82	5.41	8%	1	5.8				
ISO-SCF-32293-4	S3083F48	1235673	5.77	5.41	7%	1	5.8				FBB
ARL-83	S3084F13	163746	0.77			10	7.7	7.7			
ARL-83	S3084F14	162706	0.77			10	7.7				
ARL-83	S3084F15	164806	0.78			10	7.8				
ARL-106	S3084F16	869707	4.07			2000	8132.1	8120.1	7827.81	104%	MS-1
ARL-106	S3084F17	867360	4.06			2000	8110.2				
ARL-106	S3084F18	868206	4.06			2000	8118.1				
ISO-SCF-32293-4	S3084F19	1220899	5.70	5.41	6%	1	5.7	5.7			QC
ISO-SCF-32293-4	S3084F20	1232003	5.76	5.41	6%	1	5.8				
ISO-SCF-32293-4	S3084F21	1230936	5.75	5.41	6%	1	5.8				
ARL-84	S3084F34	33054	0.16			10	1.6	1.6			FBB
ARL-84	S3084F35	32381	0.16			10	1.6				
ARL-84	S3084F36	32300	0.16			10	1.6				

Sample Name	FILE	AREA	AMOUNT ug/mL	QC Con ug/mL	QC Bias %	Dilution Factor	Amount Sample	Avg Amt Sample	Amount Spiked	Spike Recovery	Train ID
ARL-107	S3084F37	829745	3.88			2000	7759.3	7837.5	7827.81	100%	MS-2
ARL-107	S3084F38	838117	3.92			2000	7837.4				
ARL-107	S3084F39	846508	3.96			2000	7915.7				
ISO-SCF-32293-4	S3084F40	1246426	5.82	5.41	8%	1	5.8	5.8			QC
ISO-SCF-32293-4	S3084F41	1237852	5.78	5.41	7%	1	5.8				
ISO-SCF-32293-4	S3084F42	1239959	5.79	5.41	7%	1	5.8				
ARL-85	S3085F19	75475	0.36			10	3.6	3.6			FBC
ARL-85	S3085F20	75608	0.36			10	3.6				
ARL-85	S3085F21	72681	0.35			10	3.5				
ARL-108	S3085F22	847084	3.96			2000	7921.1	7890.2	7827.81	101%	MS-3
ARL-108	S3085F23	836897	3.91			2000	7826.0				
ARL-108	S3085F24	847337	3.96			2000	7923.4				
ISO-SCF-32293-4	S3085F25	1263449	5.90	5.41	9%	1	5.9	5.9			QC
ISO-SCF-32293-4	S3085F26	1253499	5.86	5.41	8%	1	5.9				
ISO-SCF-32293-4	S3085F27	1260480	5.89	5.41	9%	1	5.9				
ARL-86	S3085F40	59577	0.29			10	2.9	2.8			FBC
ARL-86	S3085F41	56343	0.27			10	2.7				
ARL-86	S3085F42	59626	0.29			10	2.9				
ARL-109	S3085F43	851309	3.98			2000	7960.5	7944.8	7827.81	101%	MS-4
ARL-109	S3085F44	850793	3.98			2000	7955.6				
ARL-109	S3085F45	846800	3.96			2000	7918.4				
ISO-SCF-32293-4	S3085F46	1245663	5.82	5.41	8%	1	5.8	4.0			QC
ISO-SCF-32293-4	S3085F47	0	0.01	5.41	-100%	1	0.0				
ISO-SCF-32293-4	S3085F48	1296988	6.06	5.41	12%	1	6.1				
ISO-SCF-32293-4	S3088F1	1158548	5.41	5.41	0%	1	5.4				
ARL-89	S3088F2	0	0.01			10	0.1	0.1			T-RB1
ARL-89	S3088F3	0	0.01			10	0.1				
ARL-89	S3088F4	0	0.01			10	0.1				
ARL-90	S3088F5	0	0.01			10	0.1	0.1			T-RB2
ARL-90	S3088F6	5758.5	0.04			10	0.4				
ARL-90	S3088F7	5887.5	0.04			10	0.4				
ARL-91	S3088F8	0	0.01			10	0.1	0.2			T-RB3
ARL-91	S3088F9	3273	0.03			10	0.3				
ARL-91	S3088F10	0	0.01			10	0.1				

Sample Name	FILE	AREA	AMOUNT ug/mL	QC Con ug/mL	QC Dias %	Dilution Factor	Amount Sample	Avg Amt Sample	Amount Spiked	Spike Recovery	Train ID
ARL-92	S3098F11	26248	0.13			10	1.3	1.2			T-RB4
ARL-92	S3098F12	22009.08	0.12			10	1.2				
ARL-92	S3098F13	22154	0.11			10	1.1				
ISO-SCF-32293-4	S3098F14	1202.88	5.62	5.41	4%	1	5.6	5.7			QC
ISO-SCF-32293-4	S3098F15	1212015	5.66	5.41	5%	1	5.7				
ISO-SCF-32293-4	S3098F16	1220989	5.70	5.41	6%	1	5.7				
ARL-94	S3098F17	0	0.01			10	0.1	0.2			A-RB1
ARL-94	S3098F18	5431	0.04			10	0.4				
ARL-94	S3098F19	0	0.01			10	0.1				
ARL-95	S3098F20	0	0.01			10	0.1	0.1			A-RB2
ARL-95	S3098F21	0	0.01			10	0.1				
ARL-95	S3098F22	0	0.01			10	0.1				
ARL-96	S3098F23	6352.5	0.04			10	0.4	0.4			A-RB3
ARL-96	S3098F24	6436	0.04			10	0.4				
ARL-96	S3098F25	5886	0.04			10	0.4				
ARL-97	S3098F26	25808	0.13			10	1.3	0.8			A-RB4
ARL-97	S3098F27	21934	0.11			10	1.1				
ARL-97	S3098F28	0	0.01			10	0.1				
ISO-SCF-32293-4	S3098F29	1164624	5.44	5.41	1%	1	5.4	5.4			QC
ISO-SCF-32293-4	S3098F30	1159310	5.42	5.41	0%	1	5.4				
ISO-SCF-32293-4	S3098F31	1149310	5.37	5.41	-1%	1	5.4				
ARL-99	S3098F32	0	0.01			10	0.1	0.1			ABS-RB
ARL-99	S3098F33	0	0.01			10	0.1				
ARL-99	S3098F34	0	0.01			10	0.1				
ARL-100	S3098F35	0	0.01			10	0.1	0.1			ABS-RB
ARL-100	S3098F36	0	0.01			10	0.1				
ARL-100	S3098F37	0	0.01			10	0.1				
ARL-101	S3098F38	15010.13	0.08			10	0.8	0.9			ABS-RB
ARL-101	S3098F39	15823	0.08			10	0.8				
ARL-101	S3098F40	23127	0.12			10	1.2				
ARL-102	S3098F41	0	0.01			10	0.1	0.1			ABS-RB
ARL-102	S3098F42	0	0.01			10	0.1				
ARL-102	S3098F43	0	0.01			10	0.1				

Sample Name	FILE	AREA	AMOUNT ug/mL	QC Con ug/mL	QC Dias %	Dilution Factor	Amount Sample	Avg Amt Sample	Amount Spiked	Spike Recovery	Train ID
ISO-SCF-32293-4	S3098F44	1187727	5.55	5.41	3%	1	5.5	5.6			QC
ISO-SCF-32293-4	S3098F45	1189251	5.60	5.41	4%	1	5.6				
ISO-SCF-32293-4	S3098F46	1208008	5.63	5.41	4%	1	5.6				
ARL-117	S3098F47	4701	0.03			10	0.3	0.3			MB-1
ARL-117	S3098F48	4880.5	0.03			10	0.3				
ARL-117	S3098F49	5001	0.03			10	0.3				
ARL-118	S3098F50	204900	0.96			10	9.6	9.7			MB-2
ARL-118	S3098F51	207157	0.98			10	9.8				
ARL-118	S3098F52	207481	0.98			10	9.8				
ARL-119	S3098F53	446217.5	2.09			10	20.9	20.7			MB-3
ARL-119	S3098F54	427833.1	2.01			10	20.1				
ARL-119	S3098F55	452112	2.12			10	21.2				
ISO-SCF-4893-1	S3098F56	1164164	5.44	5.41	1%	1	5.4	5.5			QC
ISO-SCF-4893-1	S3098F57	1178245	5.50	5.41	2%	1	5.5				
ISO-SCF-4893-3	S3098F58	1160212	5.42	5.41	0%	1	5.4				

2.4-TDI Summary Information

Amount of 2.4-TDI Spiked into the trains: 7827.81 ug

Percent Recovery for Spiked Quad Trains

Quad No. Train ID	1		2		3		4		5		6		7		8		Average RSD
	A	B	A	B	A	B	A	B	A	B	A	B	A	B	A	B	
% Recovery	95.69%	86.19%	89.16%	95.22%	108.14%	111.93%	96.56%	97.97%	89.41%	95.59%	97.69%	99.48%	100.45%	85.83%	88.48%	83.01%	95%
Total ug	12263	11520	13258	13733	11625	12078	9694	9805	12233	12717	15471	15810	10450	9290	11197	10770	11062 16%

Amount Collected in Unspiked Quad Trains

Quad No. Train ID	1		2		3		4		5		6		7		8		Average RSD
	A	B	A	B	A	B	A	B	A	B	A	B	A	B	A	B	
Total ug	4735	4811	6287	6270	3466	3166	2132	2139	4947	5522	8042	7608	2558	2818	4088	4579	4560 41%

Percent Carry over from 1st Impinger in Spiked Quad Trains

Quad No. Train ID	1		2		3		4		5		6		7		8		Average RSD
	A	B	A	B	A	B	A	B	A	B	A	B	A	B	A	B	
1st Impinger	98.48%	99.21%	99.21%	98.97%	99.02%	99.11%	96.38%	98.46%	98.95%	99.22%	98.83%	98.71%	98.03%	97.02%	98.44%	98.35%	98.52% 0.81%
2nd Impinger	1.52%	0.79%	0.79%	1.03%	0.90%	0.89%	3.62%	1.54%	1.05%	0.78%	1.17%	1.20%	1.97%	2.88%	1.56%	1.65%	1.40% 54.38%

Percent Carry over from 1st Impinger in Unspiked Quad Trains

Quad No. Train ID	1		2		3		4		5		6		7		8		Average RSD
	A	B	A	B	A	B	A	B	A	B	A	B	A	B	A	B	
1st Impinger	99.59%	98.11%	98.81%	99.24%	99.04%	98.94%	99.14%	98.78%	99.84%	99.18%	98.69%	98.83%	98.93%	98.38%	98.51%	98.71%	98.91% 0.41%
2nd Impinger	0.41%	1.89%	1.19%	0.76%	0.96%	1.06%	0.86%	1.24%	0.38%	0.82%	1.31%	1.17%	1.07%	1.62%	1.49%	1.20%	1.09% 37.05%

AREAL WA 55 -- Method 301 Results
Using Modified Data

Run #	Train			Amount		Precision of UNSpiked Samples			
	A	B	C	D	Spiked	Diff	STDu	STDm	RSD
1	12263.0	11520.0	4735.0	4811.0	7827.81	-76.00	216.596	30.942	4.721
2	6287.0	6270.0	13258.0	13733.0	7827.81	17.00			
3	11625.0	12078.0	3466.0	3166.0	7827.81	300.00			
4	2132.0	2139.0	9694.0	9805.0	7827.81	-7.00			
5	12233.0	12717.0	4947.0	5522.0	7827.81	-575.00			
6	8084.0	7608.0	15471.0	15610.0	7827.81	476.00			
7	10450.0	9290.0	2557.0	2616.0	7827.81	-59.00			

AREAL WA 55 -- Method 301 Results
Using Modified Data

Run #	Train			Amount			Precision of Spiked Samples				Bias			
	A	B	C	D	Spiked	Diff	SDs	SDm	RSD	Run	Compound	SD	t-Test	CP
1	12263.0	11520.0	4735.0	4811.0	7827.81	743.00	430.48	162.71	3.55	-709.31	-295.41	481.90	-1.622	N/A
2	6287.0	6270.0	13258.0	13733.0	7827.81	-475.00				-610.81			^	
3	11625.0	12078.0	3466.0	3166.0	7827.81	-453.00				707.69				
4	2132.0	2139.0	9694.0	9805.0	7827.81	-111.00				-213.81			critical Value	
5	12233.0	12717.0	4947.0	5522.0	7827.81	-484.00				-587.31			is 2.160	
6	8084.0	7608.0	15471.0	15610.0	7827.81	-139.00				-133.31				
7	10450.0	9290.0	2557.0	2616.0	7827.81	1160.00				-544.31				

AREAL WA 55 -- Method 301 Results
Using Modified Data

Run #	Train			Amount		Precision of UNSpiked Samples			
	A	B	C	D	Spiked	Diff	STDu	STDm	RSD
1	12263.0	11320.0	4735.0	4811.0	7827.81	-76.00	237.150	29.644	5.205
2	6287.0	6270.0	13258.0	13733.0	7827.81	17.00			
3	11625.0	12078.0	3466.0	3166.0	7827.81	300.00			
4	2132.0	2139.0	9694.0	9805.0	7827.81	-7.00			
5	12233.0	12717.0	4947.0	5522.0	7827.81	-575.00			
6	8084.0	7600.0	15471.0	15610.0	7827.81	476.00			
7	10450.0	9290.0	2557.0	2616.0	7827.81	-59.00			
8	4086.0	4579.0	11197.0	10947.0	7827.81	-493.00			

REAL W/A 55 -- Method 301 Results
Using Modified Data

n	Train			Amount	Precision of Splked Samples					Bias				
	A	B	C		D	Splked	Diff	SDs	SDm	RSD	Run	Compound	SD	t Test
12263.0	11520.0	4735.0	4811.0	7827.81	743.00	407.50	144.07	3.40	-709.31	-394.53	471.48	-2.367	1.053	
6287.0	6270.0	13258.0	13733.0	7827.81	-475.00				-610.81					
11625.0	12076.0	3466.0	3166.0	7827.81	-453.00				707.69					
2132.0	2139.0	9694.0	9805.0	7827.81	-111.00				-213.81					
12233.0	12717.0	4947.0	5522.0	7827.81	-484.00				-587.31					
8084.0	7608.0	15471.0	15610.0	7827.81	-139.00				-133.31					
10450.0	9290.0	2557.0	2616.0	7827.81	1160.00				-544.31					
4086.0	4579.0	11197.0	10947.0	7827.81	250.00				-1088.31					

critical Value
Is 2.131

PHENOL

Phenol samples were collected using a Method 5 sampling train at 0.75 CFM using neutral-buffered absorbing reagent. The first impinger in each sampling was spiked with isotopically-labeled phenol (phenol- d_5) and 2-fluorophenol for sampling and recovery efficiency surrogates. The recovered samples were extracted and the extracts analyzed by GC/MS for phenol, phenol- d_5 and 2-fluorophenol as per EPA Method 8270. The recoveries of phenol- d_5 and 2-fluorophenol were used to adjust the measured phenol concentrations.

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COLLECTION OF SEMIVOLATILE COMPOUNDS

EPA METHOD 0010

(Interpoll Method II-8788 - Version 1.0)

EPA Method SW846 USEPA Office of Solid Waste and Emergency Response 3rd
Ed., November 1986: Test Methods for Evaluating Solid Waste Volume 2:
Field Manual Physical/Chemical Methods Method 0010.

1.0 SCOPE AND APPLICATION

1.1 This method is applicable to the determination of Destruction and Removal Efficiency (DRE) of semivolatile Principal Organic Hazardous Compounds (POHCs) from incineration systems (PHS, 1967). This method also may be used to determine particulate emission rates from stationary sources as per EPA Method 5 (see References at end of this method).

2.0 SUMMARY OF METHOD

2.1 Gaseous and particulate pollutants are withdrawn from an emission source at an isokinetic sampling rate and are collected in a multicomponent sampling train. Principal components of the train include a high-efficiency glass- or quartz-fiber filter and a packed bed of porous polymeric adsorbent resin. The filter is used to collect organic-laden particulate materials and the porous polymeric resin to adsorb semivolatile organic species. Semivolatile species are defined as compounds with boiling points $>100^{\circ}\text{C}$.

2.2 Comprehensive chemical analyses of the collected sample are conducted to determine the concentration and identity of the organic materials.

3.0 INTERFERENCES

3.1 Oxides of nitrogen (NO_x) are possible interferents in the determination of certain water-soluble compounds such as dioxane, phenol, and urethane; reaction of these compounds with NO_x in the presence of moisture will reduce their concentration. Other possibilities that could result in positive or negative bias are (1) stability of the compounds in methylene chloride, (2) the formation of water-soluble organic salts on the resin in the presence of moisture, and (3) the solvent extraction efficiency of water-soluble compounds from aqueous media. Use of two or more ions per compound for qualitative and quantitative analysis can overcome interference at one mass. These concerns should be addressed on a compound-by-compound basis before using this method.

4.0 APPARATUS AND MATERIALS

4.1 Sampling train:

4.1.1 A schematic of the sampling train used in this method is shown in Figure 1. This sampling train configuration is adapted from EPA Method 5 procedures, and, as such, the majority of the required equipment

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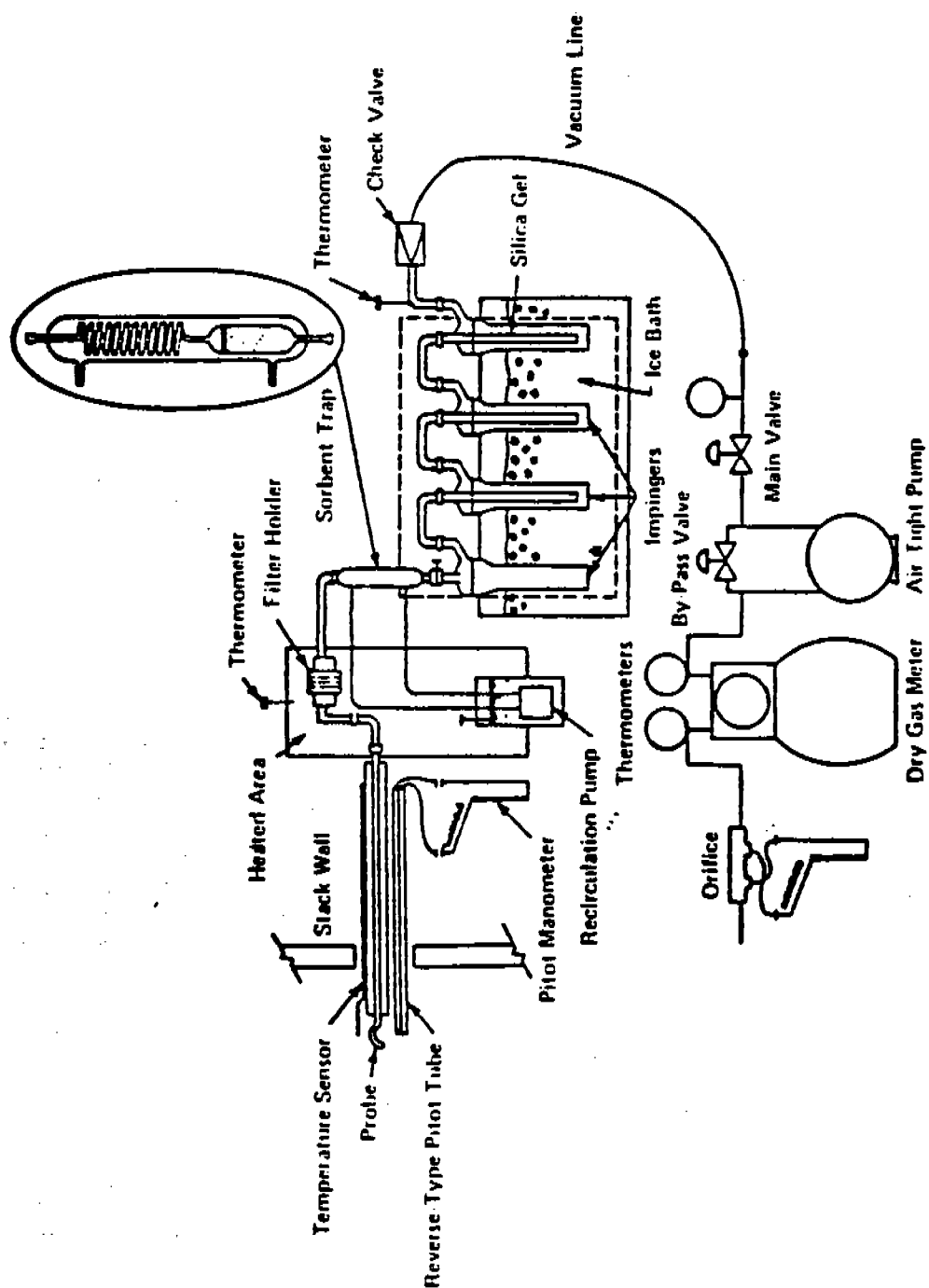


Figure 1. Modified Method 5 Sampling Train.

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is identical to that used in EPA Method 5 determinations. The new components required are a condenser coil and a sorbent module, which are used to collect semivolatile organic materials that pass through the glass- or quartz-fiber filter in the gas phase.

4.1.2 Construction details for the basic train components are given in APTD-0581 (see Martin, 1971, in Section 13.0, References); commercial models of this equipment are also available. Specifications for the sorbent module are provided in the following subsections. Additionally, the following subsections list changes to APTD-0581 and identify allowable train configuration modifications.

4.1.3 Basic operating and maintenance procedures for the sampling train are described in APTD-0576 (see Rom, 1972, in Section 13.0, References). As correct usage is important in obtaining valid results, all users should refer to APTD-0576 and adopt the operating and maintenance procedures outlined therein unless otherwise specified. The sampling train consists of the components detailed below.

4.1.3.1 Probe nozzle: Stainless steel (316) or glass with sharp, tapered (30° angle) leading edge. The taper shall be on the outside to preserve a constant I.D. The nozzle shall be buttonhook or elbow design and constructed from seamless tubing (if made of stainless steel). Other construction materials may be considered for particular applications. A range of nozzle sizes suitable for isokinetic sampling should be available in increments of 0.16 cm (1/16 in.), e.g., 0.32-1.27 cm (1/8-1/2 in.), or larger if higher volume sampling trains are used. Each nozzle shall be calibrated according to the procedures outlined in Paragraph 9.1.

4.1.3.2 Probe liner: Borosilicate or quartz-glass tubing with a heating system capable of maintaining a gas temperature of $120 \pm 14^{\circ}\text{C}$ ($248 \pm 25^{\circ}\text{F}$) at the exit end during sampling. (The tester may opt to operate the equipment at a temperature lower than that specified.) Because the actual temperature at the outlet of the probe is not usually monitored during sampling, probes constructed according to APTD-0581 and utilizing the calibration curves of APTD-0576 (or calibrated according to the procedure outlined in APTD-0576) are considered acceptable. Either borosilicate or quartz-glass probe liners may be used for stack temperatures up to about 480°C (900°F). Quartz liners shall be used for temperatures between 480 and 900°C (900 and 1650°F). (The softening temperature for borosilicate is 820°C (1508°F), and for quartz 1500°C (2732°F).) Water-cooling of the stainless steel sheath will be necessary at temperatures approaching and exceeding 500°C .

4.1.3.3 Pitot tube: Type S, as described in Section 2.1 of EPA Method 2, or other appropriate devices (Vollaro, 1976). The pitot tube shall be attached to the probe to allow constant monitoring of the stack-gas velocity. The impact (high-pressure) opening plane of the pitot tube shall be even with or above the nozzle entry plane (see EPA Method 2, Figure 2-6b) during sampling. The Type S pitot tube assembly shall have a known coefficient, determined as outlined in Section 4 of EPA Method 2.

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4.1.3.4 Differential pressure gauge: Inclined manometer or equivalent device as described in Section 2.2 of EPA Method 2. Or manometer shall be used for velocity-head (ΔP) readings and the other for orifice differential pressure (ΔH) readings.

4.1.3.5 Filter holder: Borosilicate glass, with a glass filter support and a sealing gasket. The sealing gasket should be made of materials that will not introduce organic material into the gas stream at the temperature at which the filter holder will be maintained. The gasket shall be constructed of Teflon or material of equal or better characteristics. The holder design shall provide a positive seal against leakage at any point along the filter circumference. The holder shall be attached immediately to the outlet of the cyclone or cyclone bypass.

4.1.3.6 Filter heating system: Any heating system capable of maintaining a temperature of $120 \pm 14^\circ\text{C}$ ($248 \pm 25^\circ\text{F}$) around the filter holder during sampling. Other temperatures may be appropriate for particular applications. Alternatively, the test may opt to operate the equipment at temperatures other than those specified. A temperature gauge capable of measuring temperature within 3°C (5.4°F) shall be installed so that the temperature around the filter holder can be regulated and monitored during sampling. Heating systems other than the one shown in APTD-0581 may be used.

4.1.3.7 Organic sampling module: This unit consists of three sections, including a gas-conditioning section, a sorbent trap, and a condensate knockout trap. The gas-conditioning system shall be capable of conditioning the gas leaving the back half of the filter holder to a temperature not exceeding 20°C (68°F). The sorbent trap shall be sized to contain approximately 20 g of porous polymer resin (Rohm and Haas XAD-2 or equivalent) and shall be jacketed to maintain the internal gas temperature at $17 \pm 3^\circ\text{C}$ ($62.5 \pm 5.4^\circ\text{F}$). The most commonly used coolant is ice water from the impinger ice water bath, constantly circulated through the outer jacket, using rubber or plastic tubing and a peristaltic pump. The sorbent trap should be outfitted with a glass well or depression, appropriately sized to accommodate a small thermocouple in the trap for monitoring the gas entry temperature. The condensate knockout trap shall be of sufficient size to collect the condensate following gas conditioning. The organic module components shall be oriented to direct the flow of condensate formed vertically downward from the conditioning section, through the adsorbent media, and into the condensate knockout trap. The knockout trap is usually similar in appearance to an empty impinger directly underneath the sorbent module; it may be oversized but should have a shortened center stem (at a minimum, one-half the length of the normal impinger stems) to collect a large volume of condensate without bubbling or overflowing into the impinger train. All surfaces of the organic module wetted by the gas sample shall be fabricated of borosilicate glass, Teflon, or other inert materials. Commercial versions of

complete organic module are not currently available, but may be assembled from commercially available laboratory glassware and a custom-fabricated sorbent trap. Details of two acceptable designs are shown in Figures 2 and 3 (the thermocouple well is shown in Figure 2).

4.1.3.8 Impinger train: To determine the stack-gas moisture content, four 500-mL impingers, connected in series with leak-free ground-glass joints, follow the knockout trap. The first, third, and fourth impingers shall be of the Greenburg-Smith design, modified by replacing the tip with a 1.3-cm (1/2-in.) I.D. glass tube extending about 1.3 cm (1/2 in.) from the bottom of the outer cylinder. The second impinger shall be of the Greenburg-Smith design with the standard tip. The first and second impingers shall contain known quantities of water or appropriate trapping solution. The third shall be empty or charged with a caustic solution, should the stack gas contain hydrochloric acid (HCl). The fourth shall contain a known weight of silica gel or equivalent desiccant.

4.1.3.9 Metering system: The necessary components are a vacuum gauge, leak-free pump, thermometers capable of measuring temperature to within 3°C (5.4°F), dry-gas meter capable of measuring volume to within 1%, and related equipment, as shown in Figure 1. At a minimum, the pump should be capable of 4 cfm free flow, and the dry-gas meter should have a recording capacity of 0-999.9 cu ft with a resolution of 0.005 cu ft. Other metering systems capable of maintaining sampling rates within 10% of isokineticity and of determining sample volumes to within 2% may be used. The metering system must be used in conjunction with a pitot tube to enable checks of isokinetic sampling rates. Sampling trains using metering systems designed for flow rates higher than those described in APTD-0581 and APTD-0576 may be used, provided that the specifications of this method are met.

4.1.3.10 Barometer: Mercury, aneroid, or other barometer capable of measuring atmospheric pressure to within 2.5 mm Hg (0.1 in. Hg). In many cases the barometric reading may be obtained from a nearby National Weather Service station, in which case the station value (which is the absolute barometric pressure) is requested and an adjustment for elevation differences between the weather station and sampling point is applied at a rate of minus 2.5 mm Hg (0.1 in. Hg) per 30-m (100 ft) elevation increase (vice versa for elevation decrease).

4.1.3.11 Gas density determination equipment: Temperature sensor and pressure gauge (as described in Sections 2.3 and 2.4 of EPA Method 2), and gas analyzer, if necessary (as described in EPA Method 3). The temperature sensor ideally should be permanently attached to the pitot tube or sampling probe in a fixed configuration such that the tip of the sensor extends beyond the leading edge of the probe sheath and does not touch any metal.

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~6.5 in.
or
168 mm

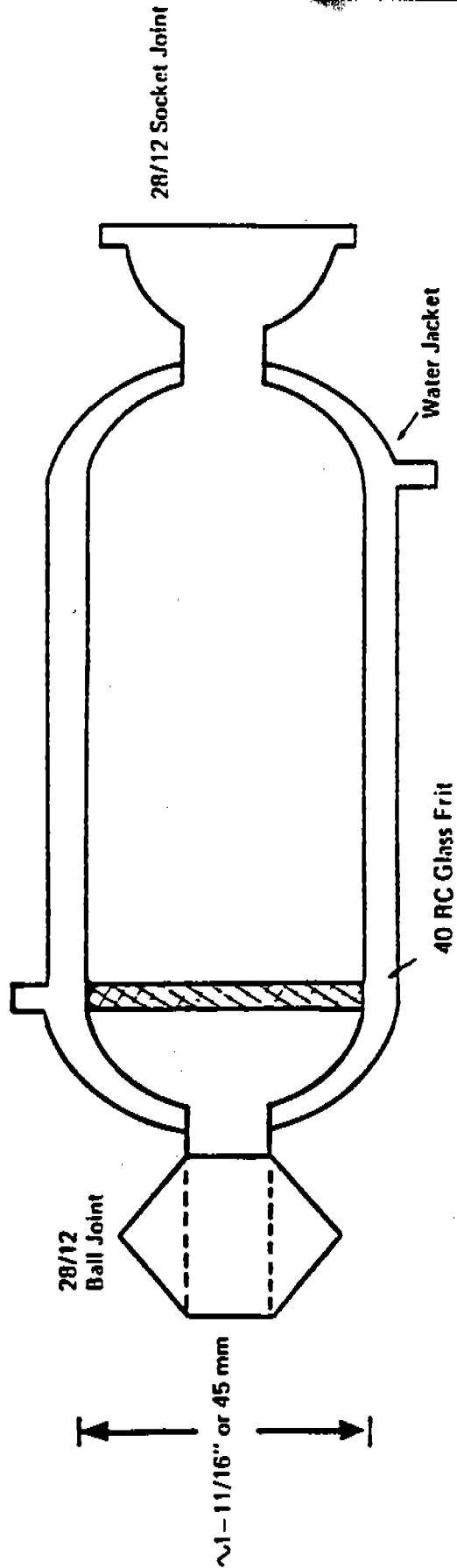


Figure 2. Adsorbent Sampling System.

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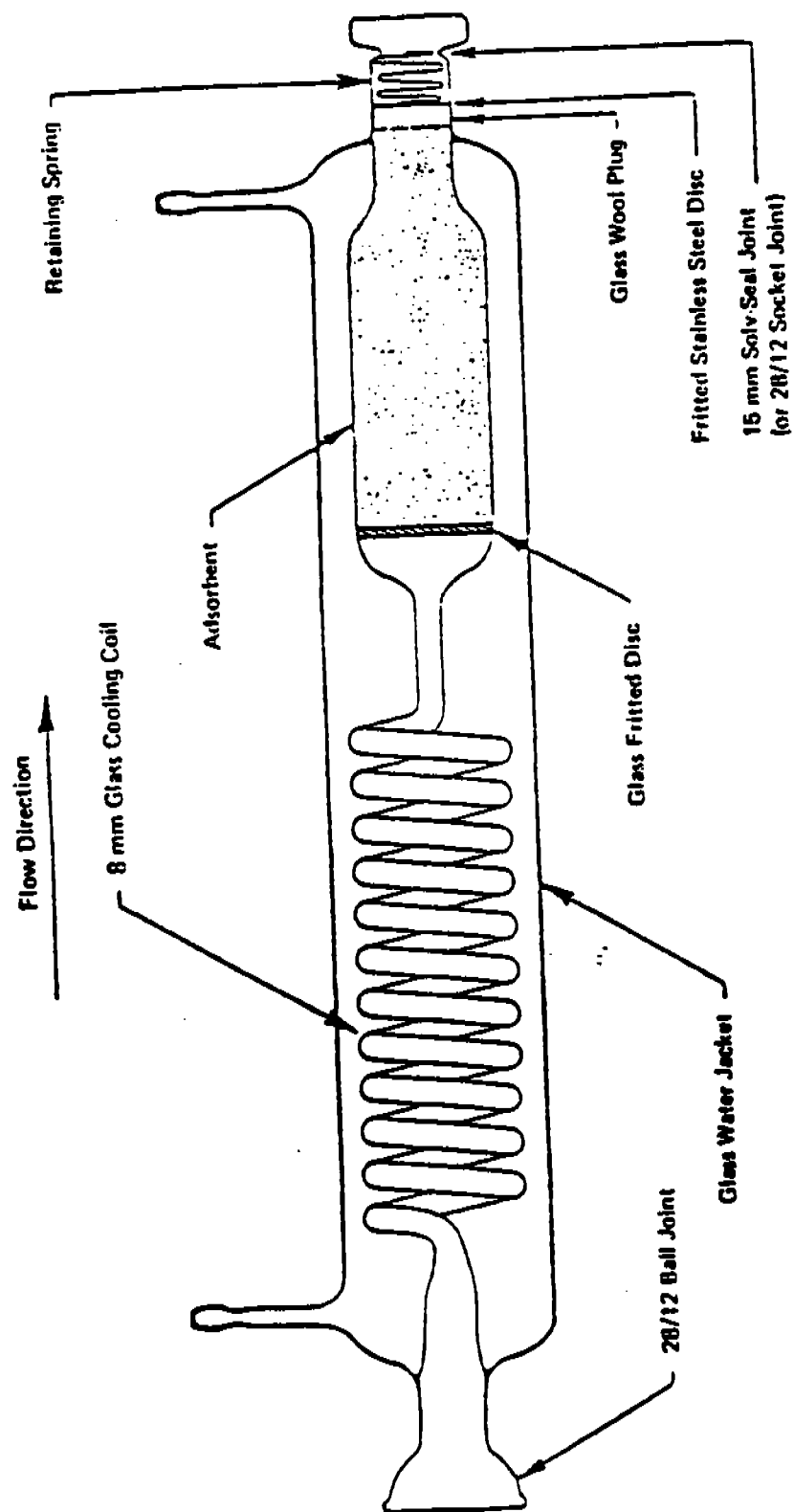


Figure 3. Adsorbent Sampling System.

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Alternatively, the sensor may be attached just prior to use in the field. Note, however, that if the temperature sensor is attached in the field, the sensor must be placed in an interference-free arrangement with respect to the Type S pitot tube openings (see EPM Method 2, Figure 2-7). As a second alternative, if a difference of no more than 1% in the average velocity measurement is to be introduced, the temperature gauge need not be attached to the probe or pitot tube.

4.1.3.12 Calibration/field-preparation record: A permanent bound laboratory notebook, in which duplicate copies of data may be made as they are being recorded, is required for documenting and recording calibrations and preparation procedures (i.e., filter and silica gel tare weights, clean XAD-2, quality assurance/quality control check results, dry-gas meter, and thermocouple calibrations, etc.). The duplicate copies should be detachable and should be stored separately in the test program archives.

4.2 Sample Recovery:

4.2.1 Probe liner: Probe nozzle and organic module conditioning section brushes; nylon bristle brushes with stainless steel wire handles are required. The probe brush shall have extensions of stainless steel, Teflon, or inert material at least as long as the probe. The brushes shall be properly sized and shaped to brush out the probe liner, the probe nozzle, and the organic module conditioning section.

4.2.2 Wash bottles: Three. Teflon or glass wash bottles are recommended; polyethylene wash bottles should not be used because organic contaminants may be extracted by exposure to organic solvents used for sample recovery.

4.2.3 Glass sample storage containers: Chemically resistant borosilicate amber and clear glass bottles, 500-mL or 1,000-mL. Bottles should be tinted to prevent action of light on sample. Screw-cap liners shall be either Teflon or constructed so as to be leak-free and resistant to chemical attack by organic recovery solvents. Narrow-mouth glass bottles have been found to exhibit less tendency toward leakage.

4.2.4 Petri dishes: Glass, sealed around the circumference with wide (1-in.) Teflon tape, for storage and transport of filter samples.

4.2.5 Graduated cylinder and/or balances: To measure condensate water to the nearest 1 mL or 1 g. Graduated cylinders shall have subdivisions not >2 mL. Laboratory triple-beam balances capable of weighing to ± 0.5 g or better are required.

4.2.6 Plastic storage containers: Screw-cap polypropylene or polyethylene containers to store silica gel.

4.2.7 Funnel and rubber policeman: To aid in transfer of silica gel to container (not necessary if silica gel is weighed in field).

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4.2.8 Funnels: Glass, to aid in sample recovery.

4.3 Filters: Glass- or quartz-fiber filters, without organic binder, exhibiting at least 99.95% efficiency ($<0.05\%$ penetration) on 0.3- μ m dioctyl hthalate smoke particles. The filter efficiency test shall be conducted in accordance with ASTM standard method D2986-71. Test data from the supplier's quality control program are sufficient for this purpose. In sources containing SO_2 or SO_3 , the filter material must be of a type that is unreactive to SO_2 or SO_3 . Reeve Angel 934 AH or Schleicher and Schwell #3 filters work well under these conditions.

4.4 Crushed ice: Quantities ranging from 10-50 lb may be necessary during a sampling run, depending on ambient air temperature.

4.5 Stopcock grease: Solvent-insoluble, heat-stable silicone grease. Use of silicone grease upstream of the module is not permitted, and amounts used on components located downstream of the organic module shall be minimized. Silicone grease usage is not necessary if screw-on connectors and Teflon sleeves or ground-glass joints are used.

4.6 Glass wool: Used to plug the unfritted end of the sorbent module. The glass-wool fiber should be solvent-extracted with methylene chloride in a Soxhlet extractor for 12 hr and air-dried prior to use.

5.0 REAGENTS

5.1 Adsorbent resin: Porous polymeric resin (XAD-2 or equivalent) is recommended. These resins shall be cleaned prior to their use for sample collection. Appendix A of this method should be consulted to determine appropriate precleaning procedure. For best results, resin used should not exhibit a blank of higher than 4 mg/kg of total chromatographable organics (TCO) (see Appendix B) prior to use. Once cleaned, resin should be stored in an airtight, wide-mouth amber glass container with a Teflon-lined cap or placed in one of the glass sorbent modules tightly sealed with Teflon film and elastic bands. The resin should be used within 4 wk of the preparation.

5.2 Silica gel: Indicating type, 6-16 mesh. If previously used, dry at 175°C (350°F) for 2 hr before using. New silica gel may be used as received. Alternatively, other types of desiccants (equivalent or better) may be used, subject to the approval of the Administrator.

5.3 Impinger solutions: Distilled organic-free water (Type II) shall be used, unless sampling is intended to quantify a particular inorganic gaseous species. If sampling is intended to quantify the concentration of additional species, the impinger solution of choice shall be subject to Administrator approval. This water should be prescreened for any compounds of interest. One hundred mL will be added to the specified impinger; the third impinger in the train may be charged with a basic solution (1 N sodium hydroxide or sodium acetate) to protect the sampling pump from acidic gases. Sodium acetate should be used when large sample volumes are anticipated because sodium hydroxide will react with carbon dioxide in aqueous media to form sodium carbonate, which may possibly plug the impinger.

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5.4 Sample recovery reagents:

5.4.1 Methylene chloride: Distilled-in-glass grade is required for sample recovery and cleanup (see Note to 5.4.2 below).

5.4.2 Methyl alcohol: Distilled-in-glass grade is required for sample recovery and cleanup.

NOTE: Organic solvents from metal containers may have a high residue blank and should not be used. Sometimes suppliers transfer solvents from metal to glass bottles; thus blanks shall be run prior to field use and only solvents with low blank value ($<0.001\%$) shall be used.

5.4.3 Water: Water (Type II) shall be used for rinsing the organic module and condenser component.

6.0 SAMPLE COLLECTION, PRESERVATION, AND HANDLING

6.1 Because of complexity of this method, field personnel should be trained in and experienced with the test procedures in order to obtain reliable results.

6.2 Laboratory preparation:

6.2.1 All the components shall be maintained and calibrated according to the procedure described in APTD-0576, unless otherwise specified.

6.2.2 Weigh several 200- to 300-g portions of silica gel in airtight containers to the nearest 0.5 g. Record on each container the total weight of the silica gel plus containers. As an alternative to preweighing the silica gel, it may instead be weighed directly in the impinger or sampling holder just prior to train assembly.

6.2.3 Check filters visually against light for irregularities and flaws or pinhole leaks. Label the shipping containers (glass Petri dishes) and keep the filters in these containers at all times except during sampling and weighing.

6.2.4 Desiccate the filters at $20 \pm 5.6^{\circ}\text{C}$ ($68 \pm 10^{\circ}\text{F}$) and ambient pressure for at least 24 hr, and weigh at intervals of at least 6 hr to a constant weight (i.e., $<0.5\text{-mg}$ change from previous weighing), recording results to the nearest 0.1 mg. During each weighing the filter must not be exposed for more than a 2-min period to the laboratory atmosphere and relative humidity above 50%. Alternatively (unless otherwise specified by the Administrator), the filters may be oven-dried at 105°C (220°F) for 2-3 hr, desiccated for 2 hr, and weighed.

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6.3 Preliminary field determinations:

6.3.1 Select the sampling site and the minimum number of sampling points according to EPA Method 1 or as specified by the Administrator. Determine the stack pressure, temperature, and range of velocity heads using EPA Method 2. It is recommended that a leak-check of the pitot lines (see EPA Method 2, Section 3.1) be performed. Determine the stack-gas moisture content using EPA Approximation Method 4 or its alternatives to establish estimates of isokinetic sampling-rate settings. Determine the stack-gas dry molecular weight, as described in EPA Method 2, Section 3.6. If integrated EPA Method 3 sampling is used for molecular weight determination, the integrated bag sample shall be taken simultaneously with, and for the same total length of time as, the sample run.

6.3.2 Select a nozzle size based on the range of velocity heads so that it is not necessary to change the nozzle size in order to maintain isokinetic sampling rates. During the run, do not change the nozzle. Ensure that the proper differential pressure gauge is chosen for the range of velocity heads encountered (see Section 2.2 of EPA Method 2).

6.3.3 Select a suitable probe liner and probe length so that all traverse points can be sampled. For large stacks, to reduce the length of the probe, consider sampling from opposite sides of the stack.

6.3.4 A minimum of 3 dscm (105.9 dscf) of sample volume is required for the determination of the Destruction and Removal Efficiency (DRE) of POHCs from incineration systems. Additional sample volume shall be collected as necessitated by analytical detection limit constraints. To determine the minimum sample volume required, refer to sample calculations in Section 10.0.

6.3.5 Determine the total length of sampling time needed to obtain the identified minimum volume by comparing the anticipated average sampling rate with the volume requirement. Allocate the same time to all traverse points defined by EPA Method 1. To avoid timekeeping errors, the length of time sampled at each traverse point should be an integer or an integer plus one-half min.

6.3.6 In some circumstances (e.g., batch cycles) it may be necessary to sample for shorter times at the traverse points and to obtain smaller gas-sample volumes. In these cases, the Administrator's approval must first be obtained.

6.4 Preparation of collection train:

6.4.1 During preparation and assembly of the sampling train, keep all openings where contamination can occur covered with Teflon film or aluminum foil until just prior to assembly or until sampling is about to begin.

6.4.2 Fill the sorbent trap section of the organic module with approximately 20 g of clean adsorbent resin. While filling, ensure that the trap packs uniformly, to eliminate the possibility of channeling. When freshly cleaned, many adsorbent resins carry a static charge, which will cause clinging to trap walls. This may be minimized by filling the trap in the presence of an antistatic device. Commercial antistatic devices include Model-204 and Model-210 manufactured by the 3M Company, St. Paul, Minnesota.

6.4.3 If an impinger train is used to collect moisture, place 100 mL of water in each of the first two impingers, leave the third impinger empty (or charge with caustic solution, as necessary), and transfer approximately 200-300 g of preweighed silica gel from its container to the fourth impinger. More silica gel may be used, but care should be taken to ensure that it is not entrained and carried out from the impinger during sampling. Place the container in a clean place for later use in the sample recovery. Alternatively, the weight of the silica gel plus impinger may be determined to the nearest 0.5 g and recorded.

6.4.4 Using a tweezer or clean disposable surgical gloves, place a labeled (identified) and weighed filter in the filter holder. Be sure that the filter is properly centered and the gasket properly placed to prevent the sample gas stream from circumventing the filter. Check the filter for tears after assembly is completed.

6.4.5 When glass liners are used, install the selected nozzle using a Viton-A O-ring when stack temperatures are $<260^{\circ}\text{C}$ (500°F) and a woven glass-fiber gasket when temperatures are higher. See APTD-0576 (Rom, 1972) for details. Other connecting systems utilizing either 316 stainless steel or Teflon ferrules may be used. When metal liners are used, install the nozzle as above, or by a leak-free direct mechanical connection. Mark the probe with heat-resistant tape or by some other method to denote the proper distance into the stack or duct for each sampling point.

6.4.6 Set up the train as in Figure 1. During assembly, do not use any silicone grease on ground-glass joints that are located upstream of the organic module. A very light coating of silicone grease may be used on all ground-glass joints that are located downstream of the organic module, but it should be limited to the outer portion (see APTD-0576) of the ground-glass joints to minimize silicone-grease contamination. Subject to the approval of the Administrator, a glass cyclone may be used between the probe and the filter holder when the total particulate catch is expected to exceed 100 mg or when water droplets are present in the stack. The organic module condenser must be maintained at a temperature of $17 \pm 3^{\circ}\text{C}$. Connect all temperature sensors to an appropriate potentiometer/display unit. Check all temperature sensors at ambient temperature.

6.4.7 Place crushed ice around the impingers and the organic module condensate knockout.

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6.4.8 Turn on the sorbent module and condenser coil coolant recirculating pump and begin monitoring the sorbent module gas entry temperature. Ensure proper sorbent module gas entry temperature before proceeding and again before any sampling is initiated. It is extremely important that the XAD-2 resin temperature never exceed 50°C (122°F), because thermal decomposition will occur. During testing, the XAD-2 temperature must not exceed 20°C (68°F) for efficient capture of the semivolatile species of interest.

6.4.9 Turn on and set the filter and probe heating systems at the desired operating temperatures. Allow time for the temperatures to stabilize.

6.5 Leak-check procedures

6.5.1 Pre-test leak-check:

6.5.1.1 Because the number of additional intercomponent connections in the Semi-VOST train (over the M5 Train) increases the possibility of leakage, a pre-test leak-check is required.

6.5.1.2 After the sampling train has been assembled, turn on and set the filter and probe heating systems at the desired operating temperatures. Allow time for the temperatures to stabilize. If a Viton A O-ring or other leak-free connection is used in assembling the probe nozzle to the probe liner, leak-check the train at the sampling site by plugging the nozzle and pulling a 381-mm Hg (15-in. Hg) vacuum.
(NOTE: A lower vacuum may be used, provided that it is not exceeded during the test.)

6.5.1.3 If an asbestos string is used, do not connect the probe to the train during the leak-check. Instead, leak-check the train by first attaching a carbon-filled leak-check impinger (shown in Figure 4) to the inlet of the filter holder (cyclone, if applicable) and then plugging the inlet and pulling a 381-mm Hg (15-in. Hg) vacuum. (Again, a lower vacuum may be used, provided that it is not exceeded during the test.) Then, connect the probe to the train and leak-check at about 25-mm Hg (1-in. Hg) vacuum; alternatively, leak-check the probe with the rest of the sampling train in one step at 381-mm Hg (15-in. Hg) vacuum. Leakage rates in excess of 4% of the average sampling rate or $>0.00057 \text{ m}^3/\text{min}$ (0.02 cfm), whichever is less, are unacceptable.

6.5.1.4 The following leak-check instructions for the sampling train described in APTD-0576 and APTD-0581 may be helpful. Start the pump with fine-adjust valve fully open and coarse-adjust valve completely closed. Partially open the coarse-adjust valve and slowly close the fine-adjust valve until the desired vacuum is reached. Do not reverse direction of the fine-adjust valve; this will cause water to back up into the organic module. If the desired vacuum is exceeded, either leak-check at this higher vacuum or end the leak-check, as shown below, and start over.

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CROSS SECTIONAL VIEW

Leak Testing Apparatus

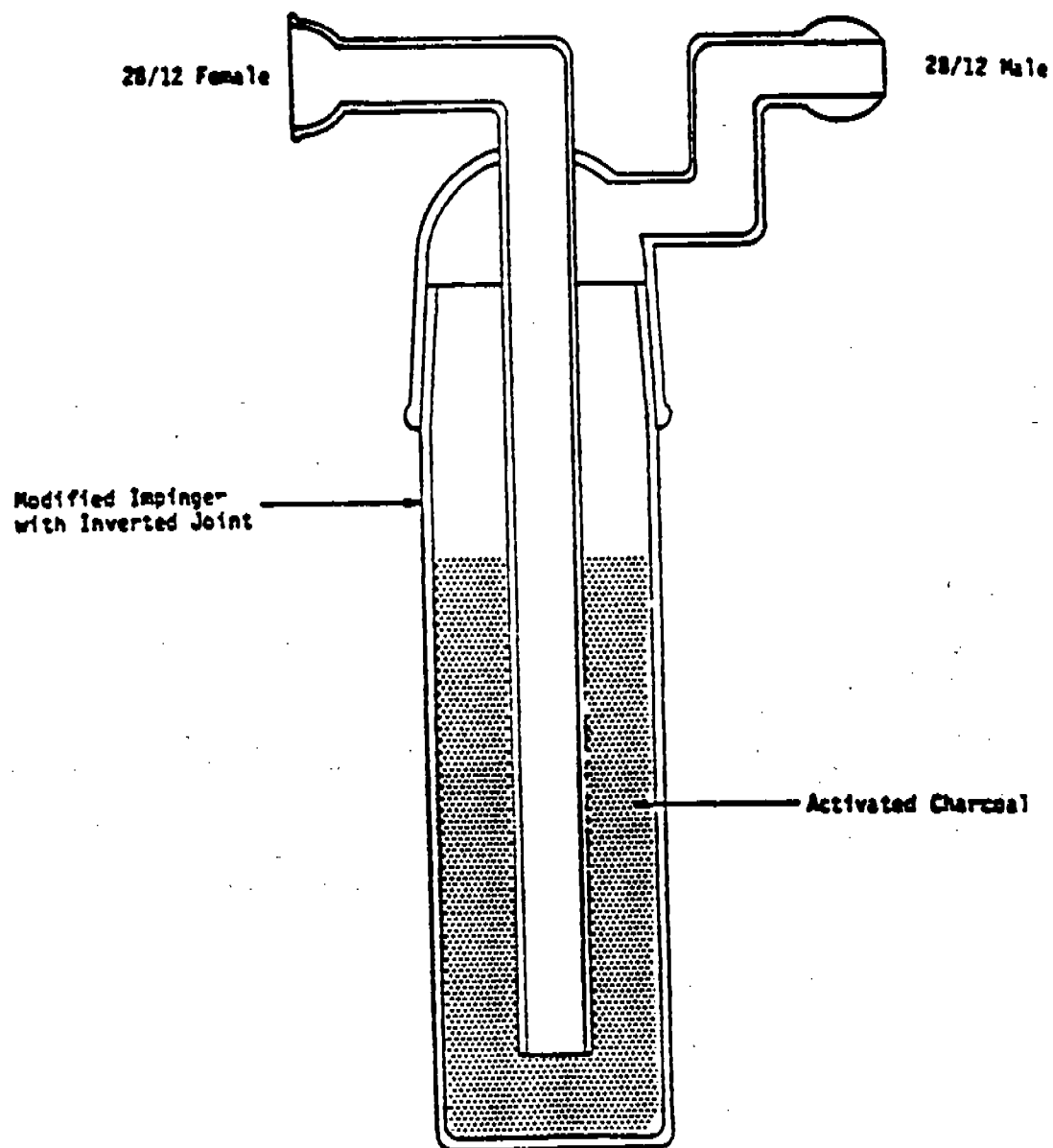


Figure 4. Leak-check impinger.

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6.5.1.5 When the leak-check is completed, first slowly remove the plug from the inlet to the probe, filter holder, or cyclone (if applicable). When the vacuum drops to 127 mm (5 in.) Hg or less, immediately close the coarse-adjust valve. Switch off the pumping system and reopen the fine-adjust valve. Do not reopen the fine-adjust valve until the coarse-adjust valve has been closed. This prevents the water in the impingers from being forced backward into the organic module and silica gel from being entrained backward into the third impinger.

6.5.2 Leak-checks during sampling run:

6.5.2.1 If, during the sampling run, a component (e.g., filter assembly, impinger, or sorbent trap) change becomes necessary, a leak-check shall be conducted immediately after the interruption of sampling and before the change is made. The leak-check shall be done according to the procedure outlined in Paragraph 6.5.1, except that it shall be done at a vacuum greater than or equal to the maximum value recorded up to that point in the test. If the leakage rate is found to be no greater than $0.00057 \text{ m}^3/\text{min}$ (0.02 cfm) or 4% of the average sampling rate (whichever is less), the results are acceptable, and no correction will need to be applied to the total volume of dry gas metered. If a higher leakage rate is obtained, the tester shall void the sampling run. (It should be noted that any "correction" of the sample volume by calculation by calculation reduces the integrity of the pollutant concentrations data generated and must be avoided.)

6.5.2.2 Immediately after a component change, and before sampling is reinitiated, a leak-check similar to a pre-test leak-check must also be conducted.

6.5.3 Post-test leak-check:

6.5.3.1 A leak-check is mandatory at the conclusion of each sampling run. The leak-check shall be done with the same procedures as those with the pre-test leak-check, except that it shall be conducted at a vacuum greater than or equal to the maximum value reached during the sampling run. If the leakage rate is found to be no greater than $0.00057 \text{ m}^3/\text{min}$ (0.02 cfm) or 4% of the average sampling rate (whichever is less), the results are acceptable, and no correction need be applied to the total volume of dry gas metered. If, however, a higher leakage rate is obtained, the tester shall either record the leakage rate, correct the sample volume (as shown in the calculation section of this method), and consider the data obtained of questionable reliability, or void the sampling run.

6.6 Sampling-train operation:

6.6.1 During the sampling run, maintain an isokinetic sampling rate to within 10% of true isokinetic, unless otherwise specified by the Administrator. Maintain a temperature around the filter of $120 \pm 14^\circ\text{C}$ ($248 \pm 25^\circ\text{F}$) and a gas temperature entering the sorbent trap at a maximum of 20°C (68°F).

6.6.2 For each run, record the data required on a data sheet such as the one shown in Figure 5. Be sure to record the initial dry-gas meter reading. Record the dry-gas meter readings at the beginning and end of each sampling time increment, when changes in flow rates are made before and after each leak-check, and when sampling is halted. Take other readings required by Figure 5 at least once at each sample point during each time increment and additional readings when significant changes (20% variation in velocity-head readings) necessitate additional adjustments in flow rate. Level and zero the manometer. Because the manometer level and zero may drift due to vibrations and temperature changes, make periodic checks during the traverse.

6.6.3 Clean the stack access ports prior to the test run to eliminate the chance of sampling deposited material. To begin sampling, remove the nozzle cap, verify that the filter and probe heating systems are at the specified temperature, and verify that the pitot tube and probe are properly positioned. Position the nozzle at the first traverse point, with the tip pointing directly into the gas stream. Immediately start the pump and adjust the flow to isokinetic conditions. Nomographs, which aid in the rapid adjustment of the isokinetic sampling rate without excessive computations, are available. These nomographs are designed for use when the Type S pitot-tube coefficient is 0.84 ± 0.02 and the stack-gas equivalent density (dry molecular weight) is equal to 29 ± 4 . APTD-0576 details the procedure for using the nomographs. If the stack-gas molecular weight and the pitot-tube coefficient are outside the above ranges, do not use the nomographs unless appropriate steps (Shigehara, 1974) are taken to compensate for the deviations.

6.6.4 When the stack is under significant negative pressure (equivalent to the height of the impinger stem), take care to close the coarse-adjust valve before inserting the probe into the stack, to prevent water from backing into the organic module. If necessary, the pump must be turned on with the coarse-adjust valve closed.

6.6.5 When the probe is in position, block off the openings around the probe and stack access port to prevent unrepresentative dilution of the gas stream.

6.6.6 Traverse the stack cross section, as required by EPA Method 1 or as specified by the Administrator, being careful not to bump the probe nozzle into the stack walls when sampling near the walls or when removing or inserting the probe through the access port, in order to minimize the chance of extracting deposited material.

6.6.7 During the test run, make periodic adjustments to keep the temperature around the filter holder and the organic module at the proper levels; add more ice and, if necessary, salt to maintain a temperature of $<20^{\circ}\text{C}$ (68°F) at the condenser/silica gel outlet. Also, periodically check the level and zero of the manometer.

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Schematic of Stock Cross Section

Figure 5. Particulate field data.

6.6.8 If the pressure drop across the filter or sorbent trap becomes too high, making isokinetic sampling difficult to maintain, the filter/sorbent trap may be replaced in the midst of a sample run. Using another complete filter holder/sorbent trap assembly is recommended, rather than attempting to change the filter and resin themselves. After a new filter/sorbent trap assembly is installed, conduct a leak-check. The total particulate weight shall include the summation of all filter assembly catches.

6.6.9 A single train shall be used for the entire sample run, except in cases where simultaneous sampling is required in two or more separate ducts or at two or more different locations within the same duct, or in cases where equipment failure necessitates a change of trains. In all other situations, the use of two or more trains will be subject to the approval of the Administrator.

6.6.10 Note that when two or more trains are used, separate analysis of the front-half (if applicable) organic-module and impinger (if applicable) catches from each train shall be performed, unless identical nozzle sizes were used on all trains. In that case, the front-half catches from the individual trains may be combined (as may the impinger catches), and one analysis of front-half catch and one analysis of impinger catch may be performed.

6.6.11 At the end of the sample run, turn off the coarse-adjust valve, remove the probe and nozzle from the stack, turn off the pump, record the final dry-gas meter reading, and conduct a post-test leak-check. Also, leak-check the pitot lines as described in EPA Method 2. The lines must pass this leak-check in order to validate the velocity-head data.

6.6.12 Calculate percent isokineticity (see Section 10.8) determine whether the run was valid or another test run should be made.

7.0 SAMPLE RECOVERY

7.1 Preparation:

7.1.1 Proper cleanup procedure begins as soon as the probe is removed from the stack at the end of the sampling period. Allow the probe to cool. When the probe can be safely handled, wipe off all external particulate matter near the tip of the probe nozzle and place a cap over the tip to prevent losing or gaining particulate matter. Do not cap the probe tip tightly while the sampling train is cooling down because this will create a vacuum in the filter holder, drawing water from the impingers into the sorbent module.

7.1.2 Before moving the sample train to the cleanup site, remove the probe from the sample train and cap the open outlet, being careful not to lose any condensate that might be present. Cap the filter inlet.

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Remove the umbilical cord from the last impinger and cap the impinger. If a flexible line is used between the organic module and the filter holder, disconnect the line at the filter holder and let any condensed water or liquid drain into the organic module.

7.1.3 Cap the filter-holder outlet and the inlet to the organic module. Separate the sorbent trap section of the organic module from the condensate knockout trap and the gas-conditioning section. Cap all organic module openings. Disconnect the organic-module knockout trap from the impinger train inlet and cap both of these openings. Ground-glass stoppers, Teflon caps, or caps of other inert materials may be used to seal all openings.

7.1.4 Transfer the probe, the filter, the organic-module components, and the impinger/condenser assembly to the cleanup area. This area should be clean and protected from the weather to minimize sample contamination or loss.

7.1.5 Save a portion of all washing solutions (methanol/methylene chloride, Type II water) used for cleanup as a blank. Transfer 200 mL of each solution directly from the wash bottle being used and place each in a separate, prelabeled glass sample container.

7.1.6 Inspect the train prior to and during disassembly and note any abnormal conditions.

7.2 Sample containers:

7.2.1 Container no. 1: Carefully remove the filter from the filter holder and place it in its identified Petri dish container. Use a pair or pairs of tweezers to handle the filter. If it is necessary to fold the filter, ensure that the particulate cake is inside the fold. Carefully transfer to the Petri dish any particulate matter or filter fibers that adhere to the filter-holder gasket, using a dry nylon bristle brush or sharp-edged blade, or both. Label the container and seal with 1-in.-wide Teflon tape around the circumference of the lid.

7.2.2 Container no. 2: Taking care that dust on the outside of the probe or other exterior surfaces does not get into the sample, quantitatively recover particulate matter or any condensate from the probe nozzle, probe fitting, probe liner, and front half of the filter holder by washing these components first with methanol/methylene chloride (1:1 v/v) into a glass container. Distilled water may also be used. Retain a water and solvent blank and analyze in the same manner as with the samples. Perform rinses as follows:

7.2.2.1 Carefully remove the probe nozzle and clean the inside surface by rinsing with the solvent mixture (1:1 v/v methanol/-methylene chloride) from a wash bottle and brushing with a nylon bristle brush. Brush until the rinse shows no visible particles; then make a final rinse of the inside surface with the solvent mix. Brush and rinse the inside parts of the Swagelok fitting with the solvent mix in a similar way until no visible particles remain.

7.2.2.2 Have two people rinse the probe liner with the solvent mix by tilting and rotating the probe while squirting solvent into its upper end so that all inside surfaces will be wetted with solvent. Let the solvent drain from the lower end into the sample container. A glass funnel may be used to aid in transferring liquid washes to the container.

7.2.2.3 Follow the solvent rinse with a probe brush. Hold the probe in an inclined position and squirt solvent into the upper end while pushing the probe brush through the probe with a twisting action; place a sample container underneath the lower end of the probe and catch any solvent and particulate matter that is brushed from the probe. Run the brush through the probe three times or more until no visible particulate matter is carried out with the solvent or until none remains in the probe liner on visual inspection. With stainless steel or other metal probes, run the brush through in the above-prescribed manner at least six times (metal probes have small crevices in which particulate matter can be entrapped). Rinse the brush with solvent and quantitatively collect these washings in the sample container. After the brushing, make a final solvent rinse of the probe as described above.

7.2.2.4 It is recommended that two people work together to clean the probe to minimize sample losses. Between sampling runs, keep brushes clean and protected from contamination.

7.2.2.5 Clean the inside of the front half of the filter holder and cyclone/cyclone flask, if used, by rubbing the surfaces with a nylon bristle brush and rinsing with methanol/methylene chloride (1:1 v/v) mixture. Rinse each surface three times or more if needed to remove visible particulate. Make a final rinse of the brush and filter holder. Carefully rinse out the glass cyclone and cyclone flask (if applicable). Brush and rinse any particulate material adhering to the inner surfaces of these components into the front-half rinse sample. After all solvent washings and particulate matter have been collected in the sample container, tighten the lid on the sample container so that solvent will not leak out when it is shipped to the laboratory. Mark the height of the fluid level to determine whether leakage occurs during transport. Label the container to identify its contents.

7.2.3 Container no. 3: The sorbent trap section of the organic module may be used as a sample transport container, or the spent resin may be transferred to a separate glass bottle for shipment. If the sorbent trap itself is used as the transport container, both ends should be sealed with tightly fitting caps or plugs. Ground-glass stoppers or Teflon caps may be used. The sorbent trap should then be labeled, covered with aluminum foil, and packaged on ice for transport to the laboratory. If a separate bottle is used, the spent resin should be quantitatively transferred from the trap into the clean bottle. Resin that adheres to the walls of the trap should be recovered using a rubber policeman or spatula and added to this bottle.

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7.2.4 Container no. 4: Measure the volume of condensate collected in the condensate knockout section of the organic module to within +1 mL by using a graduated cylinder or by weighing to within +0.5 g using a triple-beam balance. Record the volume or weight of liquid present and note any discoloration or film in the liquid catch. Transfer this liquid to a prelabeled glass sample container. Inspect the back half of the filter housing and the gas-conditioning section of the organic module. If condensate is observed, transfer it to a graduated or weighing bottle and measure the volume, as described above. Add this material to the condensate knockout-trap catch.

7.2.5 Container no. 5: All sampling train components located between the high-efficiency glass- or quartz-fiber filter and the first wet impinger or the final condenser system (including the heated Teflon line connecting the filter outlet to the condenser) should be thoroughly rinsed with methanol/methylene chloride (1:1 v/v) and the rinsings combined. This rinse shall be separated from the condensate. If the spent resin is transferred from the sorbent trap to a separate sample container for transport, the sorbent trap shall be thoroughly rinsed until all sample-wetted surfaces appear clean. Visible films should be removed by brushing. Whenever train components are brushed, the brush should be subsequently rinsed with solvent mixture and the rinsings added to this container.

7.2.6 Container no. 6: Note the color of the indicating silica gel to determine if it has been completely spent and make a notation of its condition. Transfer the silica gel from the fourth impinger to its original container and seal. A funnel may make it easier to pour the silica gel without spilling. A rubber policeman may be used as an aid in removing the silica gel from the impinger. It is not necessary to remove the small amount of dust particles that may adhere strongly to the impinger wall. Because the gain in weight is to be used for moisture calculations, do not use any water or other liquids to transfer the silica gel. If a balance is available in the field, weigh the container and its contents to 0.5 g or better.

7.3 Impinger water:

7.3.1 Make a notation of any color or film in the liquid catch. Measure the liquid in the first three impingers to within +1 mL by using a graduated cylinder or by weighing it to within +0.5 g by using a balance (if one is available). Record the volume or weight of liquid present. This information is required to calculate the moisture content of the effluent gas.

7.3.2 Discard the liquid after measuring and recording the volume or weight, unless analysis of the impinger catch is required (see Paragraph 4.1.3.7). Amber glass containers should be used for storage of impinger catch, if required.

7.3.3 If a different type of condenser is used, measure the amount of moisture condensed either volumetrically or gravimetrically.

7.4 Sample preparation for shipment: Prior to shipment, recheck all sample containers to ensure that the caps are well secured. Seal the lids of all containers around the circumference with Teflon tape. Ship all liquid samples upright on ice and all particulate filters with the particulate catch facing upward. The particulate filters should be shipped unrefrigerated.

8.0 ANALYSIS

8.1 Sample preparation:

8.1.1 General: The preparation steps for all samples will result in a finite volume of concentrated solvent. The final sample volume (usually in the 1- to 10-mL range) is then subjected to analysis by GC/MS. All samples should be inspected and the appearance documented. All samples are to be spiked with surrogate standards as received from the field prior to any sample manipulations. The spike should be at a level equivalent to 10 times the MDL when the solvent is reduced in volume to the desired level (i.e., 10 mL). The spiking compounds should be the stable isotopically labeled analog of the compounds of interest or a compound that would exhibit properties similar to the compounds of interest, be easily chromatographed, and not interfere with the analysis of the compounds of interest. Suggested surrogate spiking compounds are: deuterated naphthalene, chrysene, phenol, nitrobenzene, chlorobenzene, toluene, and carbon-13-labeled pentachlorophenol.

8.1.2 Condensate: The "condensate" is the moisture collected in the first impinger following the XAD-2 module. Spike the condensate with the surrogate standards. The volume is measured and recorded and then transferred to a separatory funnel. The pH is to be adjusted to pH 2 with 6 N sulfuric acid, if necessary. The sample container and graduated cylinder are sequentially rinsed with three successive 10-mL aliquots of the extraction solvent and added to the separatory funnel. The ratio of solvent to aqueous sample should be maintained at 1:3. Extract the sample by vigorously shaking the separatory funnel for 5 min. After complete separation of the phases, remove the solvent and transfer to a Kuderna-Danish concentrator (K-D), filtering through a bed of precleaned, dry sodium sulfate. Repeat the extraction step two additional times. Adjust the pH to 11 with 6 N sodium hydroxide and reextract combining the acid and base extracts. Rinse the sodium sulfate into the K-D with fresh solvent and discard the desiccant. Add Teflon boiling chips and concentrate to 10 mL by reducing the volume to slightly less than 10 mL and then bringing to volume with fresh solvent. In order to achieve the necessary detection limit, the sample volume can be further reduced to 1 mL by using a micro column K-D or nitrogen blow-down. Should the sample start to exhibit precipitation, the concentration step should be stopped and the sample redissolved with fresh solvent taking the volume to some finite amount. After adding a standard (for the purpose of quantitation by GC/MS), the sample is ready for analysis, as discussed in Paragraph 8.2.

8.1.3 Impinger: Spike the sample with the surrogate standards; measure and record the volume and transfer to a separatory funnel. Proceed as described in Paragraph 8.1.2.

8.1.4 XAD-2: Spike the resin directly with the surrogate standards. Transfer the resin to the all-glass thimbles by the following procedure (care should be taken so as not to contaminate the thimble by touching it with anything other than tweezers or other solvent-rinsed mechanical holding devices). Suspend the XAD-2 module directly over the thimble. The glass frit of the module (see Figure 2) should be in the up position. The thimble is contained in a clean beaker, which will serve to catch the solvent rinses. Using a Teflon squeeze bottle, flush the XAD-2 into the thimble. Thoroughly rinse the glass module with solvent into the beaker containing the thimble. Add the XAD-2 glass-wool plug to the thimble. Cover the XAD-2 in the thimble with a precleaned glass-wool plug sufficient to prevent the resin from floating into the solvent reservoir of the extractor. If the resin is wet, effective extraction can be accomplished by loosely packing the resin in the thimble. If a question arises concerning the completeness of the extraction, a second extraction, without a spike, is advised. The thimble is placed in the extractor and the rinse solvent contained in the beaker is added to the solvent reservoir. Additional solvent is added to make the reservoir approximately two-thirds full. Add Teflon boiling chips and assemble the apparatus. Adjust the heat source to cause the extractor to cycle 5-6 times per hr. Extract the resin for 16 hr. Transfer the solvent and three 10-mL rinses of the reservoir to a K-D and concentrate as described in Paragraph 8.1.2.

8.1.5 Particulate filter (and cyclone catch): If particulate loading is to be determined, weigh the filter (and cyclone catch, if applicable). The particulate filter (and cyclone catch, if applicable) is transferred to the glass thimble and extracted simultaneously with the XAD-2 resin.

8.1.6 Train solvent rinses: All train rinses (i.e., probe, impinger, filter housing) using the extraction solvent and methanol are returned to the laboratory as a single sample. If the rinses are contained in more than one container, the intended spike is divided equally among the containers proportioned from a single syringe volume. Transfer the rinse to a separatory funnel and add a sufficient amount of organic-free water so that the methylene chloride becomes immiscible and its volume no longer increases with the addition of more water. The extraction and concentration steps are then performed as described in Paragraph 8.1.2.

8.2 Sample analysis:

8.2.1 The primary analytical tool for the measurement of emissions from hazardous waste incinerators is GC/MS using fused-silica capillary GC columns, as described in Method 8270 in Chapter Four of this manual. Because of the nature of GC/MS instrumentation and the cost associated

with sample analysis, prescreening of the sample extracts by gas chromatography/flame ionization detection (GC/FID) or with electron capture (GC/ECD) is encouraged. Information regarding the complexity and concentration level of a sample prior to GC/MS analysis can be of enormous help. This information can be obtained by using either capillary columns or less expensive packed columns. However, the FID screen should be performed with a column similar to that used with the GC/MS. Keep in mind that GC/FID has a slightly lower detection limit than GC/MS and, therefore, that the concentration of the sample can be adjusted either up or down prior to analysis by GC/MS.

8.2.2 The mass spectrometer will be operated in a full scan (40-450) mode for most of the analyses. The range for which data are acquired in a GC/MS run will be sufficiently broad to encompass the major ions, as listed in Chapter Four, Method 8270, for each of the designated POHCs in an incinerator effluent analysis.

8.2.3 For most purposes, electron ionization (EI) spectra will be collected because a majority of the POHCs give reasonable EI spectra. Also, EI spectra are compatible with the NBS Library of Mass Spectra and other mass spectral references, which aid in the identification process for other components in the incinerator process streams.

8.2.4 To clarify some identifications, chemical ionization (CI) spectra using either positive ions or negative ions will be used to elucidate molecular-weight information and simplify the fragmentation patterns of some compounds. In no case, however, should CI spectra alone be used for compound identification. Refer to Chapter Four, Method 8270, for complete descriptions of GC conditions, MS conditions, and quantitative and quantitative identification.

9.0 CALIBRATION

9.1 Probe nozzle: Probe nozzles shall be calibrated before their initial use in the field. Using a micrometer, measure the inside diameter of the nozzle to the nearest 0.025 mm (0.001 in.). Make measurements at three separate places across the diameter and obtain the average of the measurements. The difference between the high and low numbers shall not exceed 0.1 mm (0.004 in.). When nozzles become nicked, dented, or corroded, they shall be reshaped, sharpened, and recalibrated before use. Each nozzle shall be permanently and uniquely identified.

9.2 Pitot tube: The Type S pitot tube assembly shall be calibrated according to the procedure outlined in Section 4 of EPA Method 2, or assigned a nominal coefficient of 0.84 if it is not visibly nicked, dented, or corroded and if it meets design and intercomponent spacing specifications.

9.3 Metering system:

9.3.1 Before its initial use in the field, the metering system shall be calibrated according to the procedure outlined in APTD-0576. Instead of physically adjusting the dry-gas meter dial readings to correspond to the wet-test meter readings, calibration factors may be used to correct the gas meter dial readings mathematically to the proper values. Before calibrating the metering system, it is suggested that a leak-check be conducted. For metering systems having diaphragm pumps, the normal leak-check procedure will not detect leakages within the pump. For these cases the following leak-check procedure is suggested: Make a 10-min calibration run at $0.00057 \text{ m}^3/\text{min}$ (0.02 cfm); at the end of the run, take the difference of the measured wet-test and dry-gas meter volumes and divide the difference by 10 to get the leak rate. The leak rate should not exceed $0.00057 \text{ m}^3/\text{min}$ (0.02 cfm).

9.3.2 After each field use, the calibration of the metering system shall be checked by performing three calibration runs at a single intermediate orifice setting (based on the previous field test). The vacuum shall be set at the maximum value reached during the test series. To adjust the vacuum, insert a valve between the wet-test meter and the inlet of the metering system. Calculate the average value of the calibration factor. If the calibration has changed by more than 5%, recalibrate the meter over the full range of orifice settings, as outlined in APTD-0576.

9.3.3 Leak-check of metering system: That portion of the sampling train from the pump to the orifice meter (see Figure 1) should be leak-checked prior to initial use and after each shipment. Leakage after the pump will result in less volume being recorded than is actually sampled. The following procedure is suggested (see Figure 6): Close the main valve on the meter box. Insert a one-hole rubber stopper with rubber tubing attached into the orifice exhaust pipe. Disconnect and vent the low side of the orifice manometer. Close off the low side orifice tap. Pressurize the system to 13-18 cm (5-7 in.) water column by blowing into the rubber tubing. Pinch off the tubing and observe the manometer for 1 min. A loss of pressure on the manometer indicates a leak in the meter box. Leaks, if present, must be corrected.

NOTE: If the dry-gas-meter coefficient values obtained before and after a test series differ by >5%, either the test series shall be voided or calculations for test series shall be performed using whichever meter coefficient value (i.e., before or after) gives the lower value of total sample volume.

9.4 Probe heater: The probe-heating system shall be calibrated before its initial use in the field according to the procedure outlined in APTD-0576. Probes constructed according to APTD-0581 need not be calibrated if the calibration curves in APTD-0576 are used.

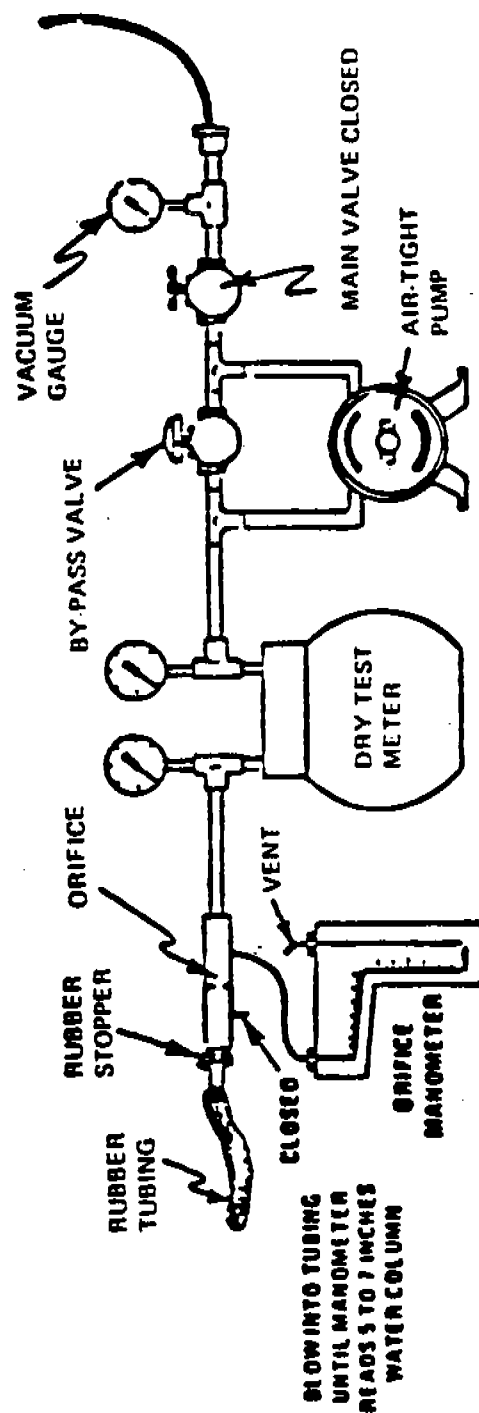


Figure 8. Leak check of meter box.

9.5 Temperature gauges: Each thermocouple must be permanently and uniquely marked on the casting; all mercury-in-glass reference thermometers must conform to ASTM E-1 63C or 63F specifications. Thermocouples should be calibrated in the laboratory with and without the use of extension leads. If extension leads are used in the field, the thermocouple readings at ambient air temperatures, with and without the extension lead, must be noted and recorded. Correction is necessary if the use of an extension lead produces a change $>1.5\%$.

9.5.1 Impinger, organic module, and dry-gas meter thermocouples: For the thermocouples used to measure the temperature of the gas leaving the impinger train and the XAD-2 resin bed, three-point calibration at ice-water, room-air, and boiling-water temperatures is necessary. Accept the thermocouples only if the readings at all three temperatures agree to $\pm 2^{\circ}\text{C}$ (3.6°F) with those of the absolute value of the reference thermometer.

9.5.2 Probe and stack thermocouple: For the thermocouples used to indicate the probe and stack temperatures, a three-point calibration at ice-water, boiling-water, and hot-oil-bath temperatures must be performed; it is recommended that room-air temperature be added, and that the thermometer and the thermocouple agree to within 1.5% at each of the calibration points. A calibration curve (equation) may be constructed (calculated) and the data extrapolated to cover the entire temperature range suggested by the manufacturer.

9.6 Barometer: Adjust the barometer initially and before each test series to agree to within ± 25 mm Hg (0.1 in. Hg) of the mercury barometer or the corrected barometric pressure value reported by a nearby National Weather Service Station (same altitude above sea level).

9.7 Triple-beam balance: Calibrate the triple-beam balance before each test series, using Class-S standard weights; the weights must be within $\pm 0.5\%$ of the standards, or the balance must be adjusted to meet these limits.

10.0 CALCULATIONS

10.1 Carry out calculations. Round off figures after the final calculation to the correct number of significant figures.

10.2 Nomenclature:

A_n = Cross-sectional area of nozzle, m^2 (ft^2).

B_{ws} = Water vapor in the gas stream, proportion by volume.

C_d = Type S pitot tube coefficient (nominally 0.84 ± 0.02), dimensionless.

I = Percent of isokinetic sampling.

- L_a = Maximum acceptable leakage rate for a leak-check, either pre-test or following a component change; equal to $0.00057 \text{ m}^3/\text{min}$ (0.02 cfm) or 4% of the average sampling rate, whichever is less.
- L_i = Individual leakage rate observed during the leak-check conducted prior to the "ith" component change ($i = 1, 2, 3 \dots n$) m^3/min (cfm).
- L_p = Leakage rate observed during the post-test leak-check, m^3/min (cfm).
- M_d = Stack-gas dry molecular weight, g/g-mole (lb/lb-mole).
- M_w = Molecular weight of water, 18.0 g/g-mole (18.0 lb/lb-mole).
- P_{bar} = Barometric pressure at the sampling site, mm Hg (in. Hg).
- P_s = Absolute stack-gas pressure, mm Hg (in. Hg).
- P_{std} = Standard absolute pressure, 760 mm Hg (29.92 in. Hg).
- R = Ideal gas constant, $0.06236 \text{ mm Hg} \cdot \text{m}^3/\text{K} \cdot \text{g-mole}$ (21.85 in. Hg-ft³/ $^{\circ}\text{R}$ -lb-mole).
- T_m = Absolute average dry-gas meter temperature (see Figure 6), K ($^{\circ}\text{R}$).
- T_s = Absolute average stack-gas temperature (see Figure 6), K ($^{\circ}\text{R}$).
- T_{std} = Standard absolute temperature, 293K (528 $^{\circ}\text{R}$).
- V_{lc} = Total volume of liquid collected in the organic module condensate knockout trap, the impingers, and silica gel, mL.
- V_m = Volume of gas sample as measured by dry-gas meter, dscm (dscf).
- $V_m(\text{std})$ = Volume of gas sample measured by the dry-gas meter, corrected to standard conditions, dscm (dscf).
- $V_w(\text{std})$ = Volume of water vapor in the gas sample, corrected to standard conditions, scm (scf).
- V_s = Stack-gas velocity, calculated by Method 2, Equation 2-9, using data obtained from Method 5, m/sec (ft/sec).
- W_a = Weight of residue in acetone wash, mg.
- γ = Dry-gas-meter calibration factor, dimensionless.
- ΔH = Average pressure differential across the orifice meter (see Figure 2), mm H₂O (in. H₂O).

ρ_w = Density of water, 0.9982 g/mL (0.002201 lb/mL).

θ = Total sampling time, min.

θ_1 = Sampling time interval from the beginning of a run until the first component change, min.

θ_i = Sampling time interval between two successive component changes, beginning with the interval between the first and second changes, min.

θ_p = Sampling time interval from the final (n^{th}) component change until the end of the sampling run, min.

13.6 = Specific gravity of mercury.

60 = sec/min.

100 = Conversion to percent.

10.3 Average dry-gas-meter temperature and average orifice pressure drop: See data sheet (Figure 5, above).

10.4 Dry-gas volume: Correct the sample measured by the dry-gas meter to standard conditions (20°C, 760 mm Hg [68°F, 29.92 in. Hg]) by using Equation 1:

$$V_{m(\text{std})} = V_m \gamma \frac{T_{\text{std}}}{T_m} \frac{P_{\text{bar}} + \Delta H/13.6}{P_{\text{std}}} = K_1 V_m \gamma \frac{P_{\text{bar}} + \Delta H/13.6}{T_m} \quad (1)$$

where:

K_1 = 0.3858 K/mm Hg for metric units, or
 K_1 = 17.64°R/in. Hg for English units.

It should be noted that Equation 1 can be used as written, unless the leakage rate observed during any of the mandatory leak-checks (i.e., the post-test leak-check or leak-checks conducted prior to component changes) exceeds L_a . If L_p or L_i exceeds L_a , Equation 1 must be modified as follows:

- a. Case I (no component changes made during sampling run): Replace V_m in Equation 1 with the expression:

$$V_m - (L_p - L_a)$$

- b. Case II (one or more component changes made during the sampling run): Replace V_m in Equation 1 by the expression:

$$V_m = (L_1 - L_a)\theta_1 - \sum_{i=2}^n (L_i - L_a)\theta_i - (L_p - L_a)\theta_p$$

and substitute only for those leakage rates (L_1 or L_p) that exceed L_a .

10.5 Volume of water vapor:

$$V_{w(std)} = V_{lc} \frac{P_w}{M_w} \frac{RT_{std}}{P_{std}} = K_2 V_{lc} \quad (2)$$

where:

$K_2 = 0.001333 \text{ m}^3/\text{mL}$ for metric units, or
 $K_2 = 0.04707 \text{ ft}^3/\text{mL}$ for English units.

10.6 Moisture content:

$$B_{ws} = \frac{V_{w(std)}}{V_{m(std)} + V_{w(std)}} \quad (3)$$

NOTE: In saturated or water-droplet-laden gas streams, two calculations of the moisture content of the stack gas shall be made, one from the impinger analysis (Equation 3) and a second from the assumption of saturated conditions. The lower of the two values of B_w shall be considered correct. The procedure for determining the moisture content based upon assumption of saturated conditions is given in the Note to Section 1.2 of Method 4. For the purposes of this method, the average stack-gas temperature from Figure 6 may be used to make this determination, provided that the accuracy of the in-stack temperature sensor is $\pm 1^\circ\text{C}$ (2°F).

10.7 Conversion factors:

From	To	Multiply by
scf	m^3	0.02832
g/ft ³	gr/ft ³	15.43
g/ft ³	lb/ft ³	2.205×10^{-3}
g/ft ³	g/m ³	35.31

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10.8 Isokinetic variation:

10.8.1 Calculation from raw data:

$$I = \frac{100 T_s [K_3 F_{lc} + (V_m/T_m) (P_{bar} + \Delta H/13.6)]}{608 V_s P_s A_n} \quad (4)$$

where:

$K_3 = 0.003454 \text{ mm Hg-m}^3/\text{mL-K}$ for metric units, or
 $K_3 = 0.002669 \text{ in. Hg-ft}^3/\text{mL-}^\circ\text{R}$ for English units.

10.8.2 Calculation for intermediate values:

$$I = \frac{T_s V_{m(std)} P_{std}^{100}}{T_{std} V_{s,std} P_{s,n} A_n B (1-B_{ws})} \quad (5)$$

$$= K_4 \frac{T_s V_{m(std)}}{P_{s,n} V_{s,std} A_n B (1-B_{ws})}$$

where:

$K_4 = 4.320$ for metric units, or
 $K_4 = 0.09450$ for English units.

10.8.3 Acceptable results: If $90\% \leq I \leq 110\%$, the results are acceptable. If the results are low in comparison with the standard and I is beyond the acceptable range, or if I is less than 90%, the Administrator may opt to accept the results.

10.9 To determine the minimum sample volume that shall be collected, the following sequence of calculations shall be used.

10.9.1 From prior analysis of the waste feed, the concentration of POHCs introduced into the combustion system can be calculated. The degree of destruction and removal efficiency that is required is used to determine the maximum amount of POHC allowed to be present in the effluent. This may be expressed as:

$$\frac{(WF) (POHC_1 \text{ conc}) (100-\%DRE)}{100} = \text{Max POHC}_1 \text{ Mass} \quad (6)$$

where:

WF = mass flow rate of waste feed per hr, g/hr (lb/hr).

POHC₁ = concentration of Principal Organic Hazardous Compound (wt %) introduced into the combustion process.

DRE = percent Destruction and Removal Efficiency required.

Max POHC = mass flow rate (g/hr [lb/hr]) of POHC emitted from the combustion source.

10.9.2 The average discharge concentration of the POHC in the effluent gas is determined by comparing the Max POHC with the volumetric flow rate being exhausted from the source. Volumetric flow rate data are available as a result of preliminary Method 1-4 determinations:

$$\frac{\text{Max POHC}_i \text{ Mass}}{\text{DV}_{\text{eff(std)}}} = \text{Max POHC}_i \text{ conc} \quad (7)$$

where:

DV_{eff(std)} = volumetric flow rate of exhaust gas, dscm (dscf).

POHC_i conc = anticipated concentration of the POHC in the exhaust gas stream, g/dscm (lb/dscf).

10.9.3 In making this calculation, it is recommended that a safety margin of at least ten be included:

$$\frac{\text{LDL}_{\text{POHC}} \times 10}{\text{POHC}_i \text{ conc}} = V_{\text{TBC}} \quad (8)$$

where:

LDL_{POHC} = detectable amount of POHC in entire sampling train.

NOTE: The whole extract from an XAD-2 cartridge is seldom if ever, injected at once. Therefore, if aliquoting factors are involved, the LDL_{POHC} is not the same as the analytical (or column) detection limit.

V_{TBC} = minimum dry standard volume to be collected at dry-gas meter.

10.10 Concentration of any given POHC in the gaseous emissions of a combustion process:

1) Multiply the concentration of the POHC as determined in Method 8270 by the final concentration volume, typically 10 mL.

$$\text{C}_{\text{POHC}} (\text{ug/mL}) \times \text{sample volume (mL)} = \text{amount (ug) of POHC in sample} \quad (9)$$

where:

CPOHC = concentration of POHC as analyzed by Method 8270.

2) Sum the amount of POHC found in all samples associated with a single train.

Total (ug) = XAD-2 (ug) + condensate (ug) + rinses (ug) + impinger (ug) (10)

3) Divide the total ug found by the volume of stack gas sampled (m³).

(Total ug)/(train sample volume) = concentration of POHC (ug/m³) (11)

11.0 QUALITY CONTROL

11.1 Sampling: See EPA Manual 600/4-77-027b for Method 5 quality control.

11.2 Analysis: The quality assurance program required for this study includes the analysis of field and method blanks, procedure validations, incorporation of stable labeled surrogate compounds, quantitation versus stable labeled internal standards, capillary column performance checks, and external performance tests. The surrogate spiking compounds selected for a particular analysis are used as primary indicators of the quality of the analytical data for a wide range of compounds and a variety of sample matrices. The assessment of combustion data, positive identification, and quantitation of the selected compounds are dependent on the integrity of the samples received and the precision and accuracy of the analytical methods employed. The quality assurance procedures for this method are designed to monitor the performance of the analytical method and to provide the required information to take corrective action if problems are observed in laboratory operations or in field sampling activities.

11.2.1 Field Blanks: Field blanks must be submitted with the samples collected at each sampling site. The field blanks include the sample bottles containing aliquots of sample recovery solvents, unused filters, and resin cartridges. At a minimum, one complete sampling train will be assembled in the field staging area, taken to the sampling area, and leak-checked at the beginning and end of the testing (or for the same total number of times as the actual test train). The filter housing and probe of the blank train will be heated during the sample test. The train will be recovered as if it were an actual test sample. No gaseous sample will be passed through the sampling train.

11.2.2 Method blanks: A method blank must be prepared for each set of analytical operations, to evaluate contamination and artifacts that can be derived from glassware, reagents, and sample handling in the laboratory.

11.2.3 Refer to Method 8270 for additional quality control considerations.

12.0 METHOD PERFORMANCE

12.1 Method performance evaluation: Evaluation of analytical procedures for a selected series of compounds must include the sample-preparation procedures and each associated analytical determination. The analytical procedures should be challenged by the test compounds spiked at appropriate levels and carried through the procedures.

12.2 Method detection limit: The overall method detection limits (lower and upper) must be determined on a compound-by-compound basis because different compounds may exhibit different collection, retention, and extraction efficiencies as well as instrumental minimum detection limit (MDL). The method detection limit must be quoted relative to a given sample volume. The upper limits for the method must be determined relative to compound retention volumes (breakthrough).

12.3 Method precision and bias: The overall method precision and bias must be determined on a compound-by-compound basis at a given concentration level. The method precision value would include a combined variability due to sampling, sample preparation, and instrumental analysis. The method bias would be dependent upon the collection, retention, and extraction efficiency of the train components. From evaluation studies to date using a dynamic spiking system, method biases of -13% and -16% have been determined for toluene and 1,1,2,2-tetrachloroethane, respectively. A precision of 19.9% was calculated from a field test data set representing seven degrees of freedom which resulted from a series of paired, unspiked Semivolatile Organic Sampling trains (Semi-VOST) sampling emissions from a hazardous waste incinerator.

13.0 REFERENCES

1. Addendum to Specifications for Incinerator Testing at Federal Facilities, PHS, NCAPC, December 6, 1967.
2. Bursey, J., Homolya, J., McAllister, R., and McGangley, J., Laboratory and Field Evaluation of the Semi-VOST Method, Vols. 1 and 2, U.S. Environmental Protection Agency, EPA/600/4-851/075A, 075B (1985).
3. Martin, R.M., Construction Details of Isokinetic Source-Sampling Equipment, Research Triangle Park, NC, U.S. Environmental Protection Agency, April 1971, PB-203 060/BE, APTD-0581, 35 pp.
4. Rom, J.J., Maintenance, Calibration, and Operation of Isokinetic Source-Sampling Equipment, Research Triangle Park, NC, U.S. Environmental Protection Agency, March 1972, PB-209 022/BE, APTD-0576, 39 pp.
5. Schlickerrieder, L.M., Adams, J.W., and Thrun, K.E., Modified Method 5 Train and Source Assessment Sampling System: Operator's Manual, U.S. Environmental Protection Agency, EPA/600/8-85/003, (1985).

6. Shigehara, R.T., Adjustments in the EPA Nomography for Different Pitot Tube Coefficients and Dry Molecular Weights, Stack Sampling News, 2:4-11 (October 1974).

7. U.S. Environmental Protection Agency, CFR 40 Part 60, Appendix A, Methods 1-5.

8. Vollaro, R.F., A Survey of Commercially Available Instrumentation for the Measurement of Low-Range Gas Velocities, Research Triangle Park, NC, U.S. Environmental Protection Agency, Emissions Measurement Branch, November 1976 (unpublished paper).

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PREPARATION OF XAD-2 SORBENT RESIN

1.0 SCOPE AND APPLICATION

1.1 XAD-2 resin as supplied by the manufacturer is impregnated with a bicarbonate solution to inhibit microbial growth during storage. Both the salt solution and any residual extractable monomer and polymer species must be removed before use. The resin is prepared by a series of water and organic extractions, followed by careful drying.

2.0 EXTRACTION

2.1 Method 1: The procedure may be carried out in a giant Soxhlet extractor. An all-glass thimble containing an extra-coarse frit is used for extraction of XAD-2. The frit is recessed 10-15 mm above a crenellated ring at the bottom of the thimble to facilitate drainage. The resin must be carefully retained in the extractor cup with a glass-wool plug and stainless steel screen because it floats on methylene chloride. This process involves sequential extraction in the following order.

<u>Solvent</u>	<u>Procedure</u>
Water	Initial rinse: Place resin in a beaker, rinse once with Type II water, and discard. Fill with water a second time, let stand overnight, and discard.
Water	Extract with H ₂ O for 8 hr.
Methyl alcohol	Extract for 22 hr.
Methylene chloride	Extract for 22 hr.
Methylene chloride (fresh)	Extract for 22 hr.

2.2 Method 2:

2.2.1 As an alternative to Soxhlet extraction, a continuous extractor has been fabricated for the extraction sequence. This extractor has been found to be acceptable. The particular canister used for the apparatus shown in Figure A-1 contains about 500 g of finished XAD-2. Any size may be constructed; the choice is dependent on the needs of the sampling programs. The XAD-2 is held under light spring tension between a pair of coarse and fine screens. Spacers under the bottom screen allow for even distribution of clean solvent. The three-necked flask should be of sufficient size (3-liter in this case) to hold solvent

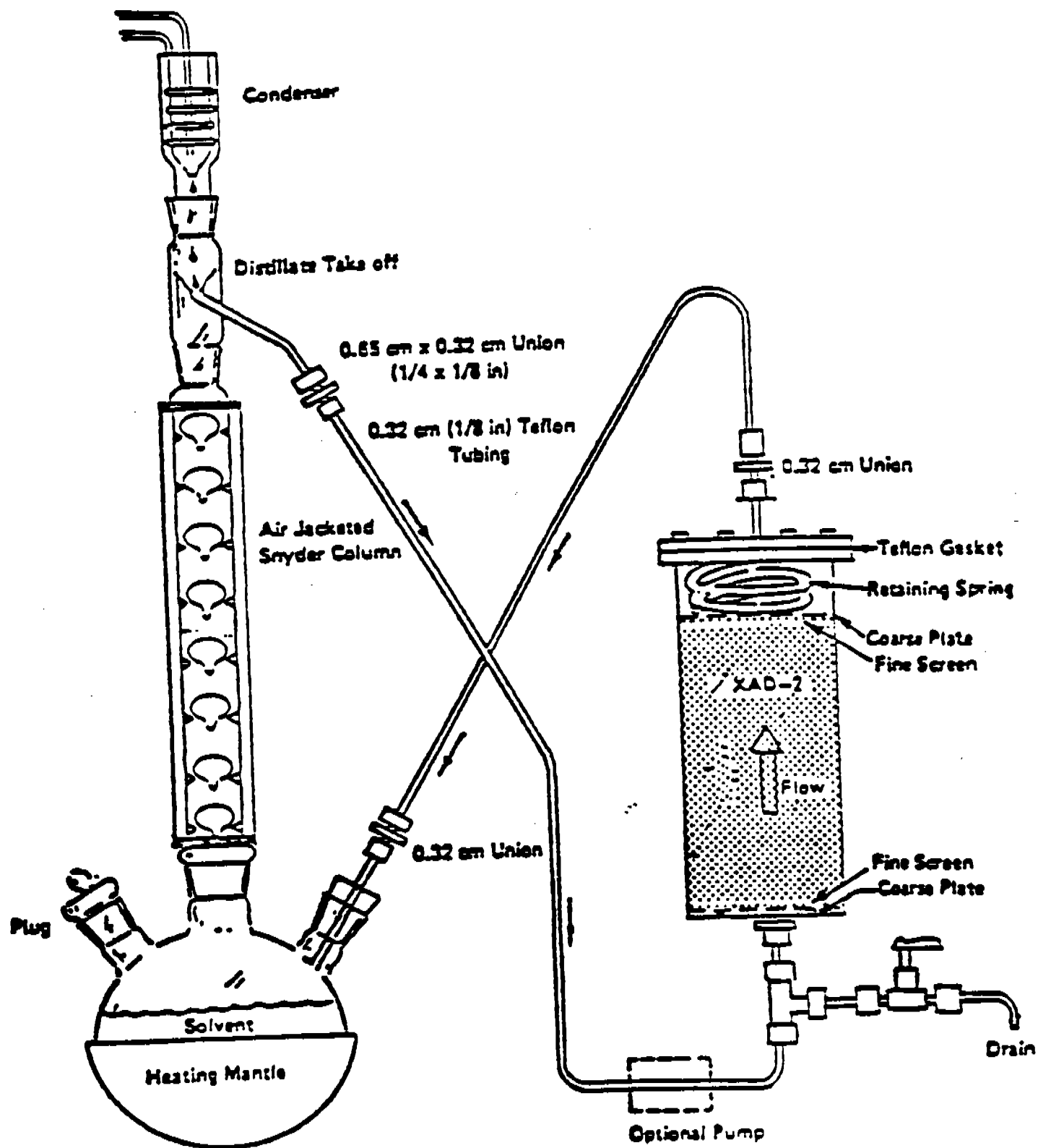


Figure A-1. XAD-2 cleanup extraction apparatus.

equal to twice the dead volume of the XAD-2 canister. Solvent is refluxed through the Snyder column, and the distillate is continuously cycled up through the XAD-2 for extraction and returned to the flask. The flow is maintained upward through the XAD-2 to allow maximum solvent contact and prevent channeling. A valve at the bottom of the canister allows removal of solvent from the canister between changes.

2.2.2 Experience has shown that it is very difficult to cycle sufficient water in this mode. Therefore the aqueous rinse is accomplished by simply flushing the canister with about 20 liters of distilled water. A small pump may be useful for pumping the water through the canister. The water extraction should be carried out at the rate of about 20-40 mL/min.

2.2.3 After draining the water, subsequent methyl alcohol and methylene chloride extractions are carried out using the refluxing apparatus. An overnight or 10- to 20-hr period is normally sufficient for each extraction.

2.2.4 All materials of construction are glass, Teflon, or stainless steel. Pumps, if used, should not contain extractable materials. Pumps are not used with methanol and methylene chloride.

3.0 DRYING

3.1 After evaluation of several methods of removing residual solvent, a fluidized-bed technique has proved to be the fastest and most reliable drying method.

3.2 A simple column with suitable retainers, as shown in Figure A-2, will serve as a satisfactory column. A 10.2-cm (4-in.) Pyrex pipe 0.6 m (2 ft) long will hold all of the XAD-2 from the extractor shown in Figure A-1 or the Soxhlet extractor, with sufficient space for fluidizing the bed while generating a minimum resin load at the exit of the column.

3.3 Method 1: The gas used to remove the solvent is the key to preserving the cleanliness of the XAD-2. Liquid nitrogen from a standard commercial liquid nitrogen cylinder has routinely proved to be a reliable source of large volumes of gas free from organic contaminants. The liquid nitrogen cylinder is connected to the column by a length of precleaned 0.95-cm (3/8-in.) copper tubing, coiled to pass through a heat source. As nitrogen is bled from the cylinder, it is vaporized in the heat source and passes through the column. A convenient heat source is a water bath heated from a steam line. The final nitrogen temperature should only be warm to the touch and not over 40°C. Experience has shown that about 500 g of XAD-2 may be dried overnight by consuming a full 160-liter cylinder of liquid nitrogen.

3.4 Method 2: As a second choice, high-purity tank nitrogen may be used to dry the XAD-2. The high-purity nitrogen must first be passed through a bed

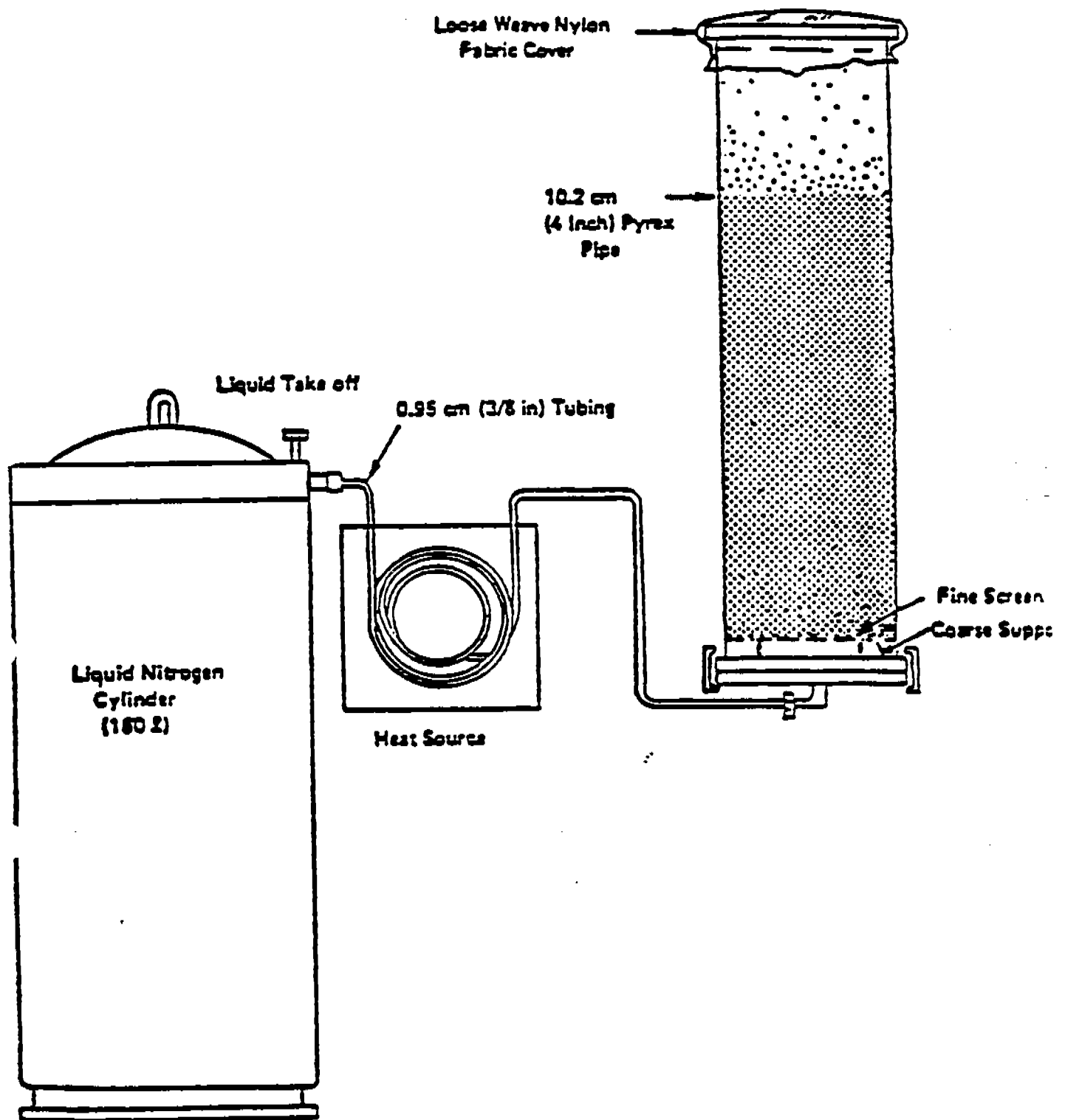


Figure A-2. XAD-2 fluidized-bed drying apparatus.

of activated charcoal approximately 150 mL in volume. With either type of drying method, the rate of flow should gently agitate the bed. Excessive fluidization may cause the particles to break up.

4.0 QUALITY CONTROL PROCEDURES

4.1 For both Methods 1 and 2, the quality control results must be reported for the batch. The batch must be reextracted if the residual extractable organics are >20 ug/mL by TCO analysis or the gravimetric residue is >0.5 mg/20 g XAD-2 extracted. (See also section 5.1, Method 0010.)

4.2 Four control procedures are used with the final XAD-2 to check for (1) residual methylene chloride, (2) extractable organics (TCO), (3) specific compounds of interest as determined by GC/MS, as described in Section 4.5 below, and (4) residue (GRAV).

4.3 Procedure for residual methylene chloride:

4.3.1 Description: A 1 ± 0.1 -g sample of dried resin is weighed into a small vial, 3 mL of toluene are added, and the vial is capped and well shaken. Five μ L of toluene (now containing extracted methylene chloride) are injected into a gas chromatograph, and the resulting integrated area is compared with a reference standard. The reference solution consists of 2.5 μ L of methylene chloride in 100 mL of toluene, simulating 100 ug of residual methylene chloride on the resin. The acceptable maximum content is 1,000 ug/g resin.

4.3.2 Experimental: The gas chromatograph conditions are as follows:

6-ft x 1/8-in. stainless steel column containing 10% OV-101 on 100/120 Supelcoport;

Helium carrier at 30 mL/min;

FID operated on 4×10^{-11} A/mV;

Injection port temperature: 250°C;

Detector temperature: 305°C;

Program: 30°C(4 min) 40°C/min 250°C (hold); and

Program terminated at 1,000 sec.

4.4 Procedure for residual extractable organics:

4.4.1 Description: A 20 ± 0.1 -g sample of cleaned, dried resin is weighed into a precleaned alundum or cellulose thimble which is plugged with cleaned glass wool. (Note that 20 g of resin will fill a thimble, and the

TOTAL CHROMATOGRAPHABLE ORGANIC MATERIAL ANALYSIS

1.0 SCOPE AND APPLICATION

1.1 In this procedure, gas chromatography is used to determine the quantity of lower boiling hydrocarbons (boiling points between 90° and 300°C) in the concentrates of all organic solvent rinses, XAD-2 resin and LC fractions - when Method 1 is used (see References, Method 0010) - encountered in Level 1 environmental sample analyses. Data obtained using this procedure serve a twofold purpose. First, the total quantity of the lower boiling hydrocarbons in the sample is determined. Then whenever the hydrocarbon concentrations in the original concentrates exceed 75 ug/m³, the chromatography results are reexamined to determine the amounts of individual species.

The extent of compound identification is limited to representing all materials as normal alkanes based upon comparison of boiling points. Thus the method is not qualitative. In a similar manner, the analysis is semiquantitative; calibrations are prepared using only one hydrocarbon. They are replicated but samples routinely are not.

1.2 Application: This procedure applies solely to the Level 1 C7-C16 gas chromatographic analysis of concentrates of organic extracts, neat liquids, and of LC fractions. Throughout the procedure, it is assumed the analyst has been given a properly prepared sample.

1.3 Sensitivity: The sensitivity of this procedure, defined as the slope of a plot of response versus concentration, is dependent on the instrument and must be verified regularly. TRW experience indicates the nominal range is of the order of 77 uV·V·sec·uL/ng of n-heptane and 79 uV·sec·uL/ng of n-hexadecane. The instrument is capable of perhaps one hundredfold greater sensitivity. The level specified here is sufficient for Level 1 analysis.

1.4 Detection limit: The detection limit of this procedure as written is 1.3 ng/uL for a 1 uL injection of n-decane. This limit is arbitrarily based on defining the minimum detectable response as 100 uV·sec. This is an easier operational definition than defining the minimum detection limit to be that amount of material which yields a signal twice the noise level.

1.5 Range: The range of the procedure will be concentrations of 1.3 ng/uL and greater.

1.6 Limitations

1.6.1 Reporting limitations: It should be noted that a typical environmental sample will contain compounds which: (a) will not elute in the specified boiling ranges and thus will not be reported, and/or (b)

resin will float out unless well plugged.) The thimble containing the resin is extracted for 24 hr with 200-mL of pesticide-grade methylene chloride (Burdick and Jackson pesticide-grade or equivalent purity). The 200-mL extract is reduced in volume to 10-mL using a Kuderna-Danish concentrator and/or a nitrogen evaporation stream. Five μ L of that solution are analyzed by gas chromatography using the TCO analysis procedure. The concentrated solution should not contain >20 μ g/mL of TCO extracted from the XAD-2. This is equivalent to 10 μ g/g of TCO in the XAD-2 and would correspond to 1.3 mg of TCO in the extract of the 130-g XAD-2 module. Care should be taken to correct the TCO data for a solvent blank prepared (200 mL reduced to 10 mL) in a similar manner.

4.4.2 Experimental: Use the TCO analysis conditions described in the revised Level 1 manual (EPA 600/7-78-201).

4.5 GC/MS Screen: The extract, as prepared in paragraph 4.4.1, is subjected to GC/MS analysis for each of the individual compounds of interest. The GC/MS procedure is described in Chapter Four, Method 8270. The extract is screened at the MDL of each compound. The presence of any compound at a concentration >25 μ g/mL in the concentrated extract will require the XAD-2 to be recleaned by repeating the methylene chloride step.

4.6 Methodology for residual gravimetric determination: After the TCO value and GC/MS data are obtained for the resin batch by the above procedures, dry the remainder of the extract in a tared vessel. There must be <0.5 mg residue registered or the batch of resin will have to be extracted with fresh methylene chloride again until it meets this criterion. This level corresponds to 25 μ g/g in the XAD-2, or about 3.25 mg in a resin charge of 130 g.

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will not elute from the column at all and thus will not be reported. Consequently, the organic content of the sample as reported is a lower bound and should be regarded as such.

1.6.2 Calibration limitations: Quantitation is based on calibration with n-decane. Data should therefore be reported as, e.g., mg C₈/m³ as n-decane. Since response varies linearly with carbon number (over a wide range the assumption may involve a 20% error), it is clear that heptane (C₇) detected in a sample and quantitated as decane will be overestimated. Likewise, hexadecane (C₁₆) quantitated as decane will be underestimated. From previous data, it is estimated the error involved is on the order of 6-7%.

1.6.3 Detection limitations: The sensitivity of the flame ionization detector varies from compound to compound. However, n-alkanes have a greater response than other classes. Consequently, using an n-alkane as a calibrant and assuming equal responses of all other compounds tends to give low reported values.

2.0 SUMMARY OF METHOD

2.1 A mL aliquot of all 10-mL concentrates is disbursed for GC-TCO analysis. With boiling point-retention time and response-amount calibration curves, the data (peak retention times and peak areas) are interpreted by first summing peak areas in the ranges obtained from the boiling point-retention time calibration. Then, with the response-amount calibration curve, the area sums are converted to amounts of material in the reported boiling point ranges.

2.2 After the instrument is set up, the boiling point-retention time calibration is effected by injecting a mixture of n-C₇ through n-C₁₆ hydrocarbons and operating the standard temperature program. Response-quantity calibrations are accomplished by injecting n-decane in n-pentane standards and performing the standard temperature program.

2.3 Definitions

2.3.1 GC: Gas chromatography or gas chromatograph.

2.3.2 C₇-C₁₆ n-alkanes: Heptane through hexadecane.

2.3.3 GCA temperature program: 4 min isothermal at 60°C, 10°C/min from 60° to 220°C.

2.3.4 TRW temperature program: 5 min isothermal at room temperature, then program from 30°C to 250°C at 15°C/min.

3.0 INTERFERENCES

Not applicable.

4.0 APPARATUS AND MATERIALS

4.1 Gas chromatograph: This procedure is intended for use on a Varian 1860 gas chromatograph, equipped with dual flame ionization detectors and a linear temperature programmer. Any equivalent instrument can be used provided that electrometer settings, etc., be changed appropriately.

4.2 Gases:

4.2.1 Helium: Minimum quality is reactor grade. A 4A or 13X molecular sieve drying tube is required. A filter must be placed between the trap and the instrument. The trap should be recharged after every third tank of helium.

4.2.2 Air: Zero grade is satisfactory.

4.2.3 Hydrogen: Zero grade.

4.3 Syringe: Syringes are Hamilton 701N, 10 uL, or equivalent.

4.4 Septa: Septa will be of such quality as to produce very low bleed during the temperature program. An appropriate septum is Supelco Microsep 138, which is Teflon-backed. If septum bleed cannot be reduced to a negligible level, it will be necessary to install septum swingers on the instrument.

4.5 Recorder: The recorder of this procedure must be capable of not less than 1 mV full-scale display, a 1-sec time constant and 0.5 in. per min chart rate.

4.6 Integrator: An integrator is required. Peak area measurement by hand is satisfactory but too time-consuming. If manual integration is required, the method of "height times width at half height" is used.

4.7 Columns:

4.7.1 Preferred column: 6 ft x 1/8 in. O.D. stainless steel column of 10% OV-101 on 100/120 mesh Supelcoport.

4.7.2 Alternate column: 6 ft x 1/8 in. O.D. stainless steel column of 10% OV-1 (or other silicon phase) on 100/120 mesh Supelcoport.

4.8 Syringe cleaner: Hamilton syringe cleaner or equivalent connected to a suitable vacuum source.

5.0 REAGENTS

5.1 Pentane: "Distilled-in-Glass" (reg. trademark) or "Nanograde" (reg. trademark) for standards and for syringe cleaning.

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5.2 Methylene chloride: "Distilled-in-Glass" (reg. trademark) or "Nanograde" (reg. trademark) for syringe cleaning.

6.0 SAMPLING HANDLING AND PRESERVATION

6.1 The extracts are concentrated in a Kuderna-Danish evaporator to a volume less than 10 mL. The concentrate is then quantitatively transferred to a 10-mL volumetric flask and diluted to volume. A 1-mL aliquot is taken for both this analysis and possible subsequent GC/MS analysis and set aside in the sample bank. For each GC-TCO analysis, obtain the sample sufficiently in advance to allow it to warm to room temperature. For example, after one analysis is started, return that sample to the sample bank and take the next sample.

7.0 PROCEDURES

7.1 Setup and checkout: Each day, the operator will verify the following:

7.1.1 That supplies of carrier gas, air and hydrogen are sufficient, i.e., that each tank contains > 100 psig.

7.1.2 That, after replacement of any gas cylinder, all connections leading to the chromatograph have been leak-checked.

7.1.3 That the carrier gas flow rate is 30 ± 2 mL/min, the hydrogen flow rate is 30 ± 2 mL/min, and the air flow rate is 300 ± 20 mL/min.

7.1.4 That the electrometer is functioning properly.

7.1.5 That the recorder and integrator are functioning properly.

7.1.6 That the septa have been leak-checked (leak-checking is effected by placing the soap bubble flow meter inlet tube over the injection port adaptors), and that no septum will be used for more than 20 injections.

7.1.7 That the list of samples to be run is ready.

7.2 Retention time calibration:

7.2.1 To obtain the temperature ranges for reporting the results of the analyses, the chromatograph is given a normal boiling point-retention time calibration. The n-alkanes, their boiling points, and data reporting ranges are given in the table below:

	<u>NBP, °C</u>	<u>Reporting Range, °C</u>	<u>Report As</u>
n-heptane	98	90-110	C7
n-octane	126	110-140	C8
n-nonane	151	140-160	C9
n-decane	174	160-180	C10
n-undecane	194	180-200	C11
n-dodecane	214	200-220	C12
n-tridecane	234	220-240	C13
n-tetradecane	252	240-260	C14
n-pentadecane	270	260-280	C15
n-hexadecane	288	280-300	C16

7.2.2 Preparation of standards: Preparing a mixture of the C7-C16 alkanes is required. There are two approaches: (1) use of a standards kit (e.g., Polyscience Kit) containing bottles of mixtures of selected n-alkanes which may be combined to produce a C7-C16 standard; or (2) use of bottles of the individual C7-C16 alkanes from which accurately known volumes may be taken and combined to give a C7-C16 mixture.

7.2.3 Procedure for retention time calibration: This calibration is performed at the start of an analytical program; the mixture is chromatographed at the start of each day. To attain the required retention time precision, both the carrier gas flow rate and the temperature program specifications must be observed. Details of the procedure depend on the instrument being used. The general procedure is as follows:

7.2.3.1 Set the programmer upper limit at 250°C. If this setting does not produce a column temperature of 250°C, find the correct setting.

7.2.3.2 Set the programmer lower limit at 30°C.

7.2.3.3 Verify that the instrument and samples are at room temperature.

7.2.3.4 Inject 1 µL of the n-alkane mixture.

7.2.3.5 Start the integrator and recorder.

7.2.3.6 Allow the instrument to run isothermally at room temperature for five min.

7.2.3.7 Shut the oven door.

7.2.3.8 Change the mode to Automatic and start the temperature program.

7.2.3.9 Repeat Steps 1-9 a sufficient number of times so that the relative standard deviation of the retention times for each peak is <5%.

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7.3 Response calibration:

7.3.1 For the purposes of a Level 1 analysis, response-quantity calibration with n-decane is adequate. A 10- μ L volume of n-decane is injected into a tared 10 mL volumetric flask. The weight injected is obtained and the flask is diluted to the mark with n-pentane. This standard contains about 730 ng n-decane per μ L n-pentane. The exact concentration depends on temperature, so that a weight is required. Two serial tenfold dilutions are made from this standard, giving standards at about 730, 73, and 7.3 ng n-decane per μ L n-pentane, respectively.

7.3.2 Procedure for response calibration: This calibration is performed at the start of an analytical program and monthly thereafter. The most concentrated standard is injected once each day. Any change in calibration necessitates a full calibration with new standards. Standards are stored in the refrigerator locker and are made up monthly.

7.3.2.1 Verify that the instrument is set up properly.

7.3.2.2 Set electrometer at 1×10^{-10} A/mV.

7.3.2.3 Inject 1 μ L of the highest concentration standard.

7.3.2.4 Run standard temperature program as specified above.

7.3.2.5 Clean syringe.

7.3.2.6 Make repeated injections of all three standards until the relative standard deviations of the areas of each standard are $\leq 5\%$.

7.4 Sample analysis procedure:

7.4.1 The following apparatus is required:

7.4.1.1 Gas chromatograph set up and working.

7.4.1.2 Recorder, integrator working.

7.4.1.3 Syringe and syringe cleaning apparatus.

7.4.1.4 Parameters: Electrometer setting is 1×10^{-10} A/mV; recorder is set at 0.5 in./min and 1 mV full-scale.

7.4.2 Steps in the procedure are:

7.4.2.1 Label chromatogram with the data, sample number, etc.

7.4.2.2 Inject sample.

7.4.2.3 Start integrator and recorder.

7.4.2.4 After isothermal operation for 5 min, begin temperature program.

7.4.2.5 Clean syringe.

7.4.2.6 Return sample; obtain new sample.

7.4.2.7 When analysis is finished, allow instrument to cool. Turn chromatogram and integrator output and data sheet over to data analyst.

7.5 Syringe cleaning procedure:

7.5.1 Remove plunger from syringe.

7.5.2 Insert syringe into cleaner; turn on aspirator.

7.5.3 Fill pipet with pentane; run pentane through syringe.

7.5.4 Repeat with methylene chloride from a separate pipet.

7.5.5 Flush plunger with pentane followed by methylene chloride.

7.5.6 Repeat with methylene chloride.

7.6 Sample analysis decision criterion: The data from the TCO analyses of organic extract and rinse concentrates are first used to calculate the total concentration of C7-C16 hydrocarbon-equivalents (Paragraph 7.7.3) in the sample with respect to the volume of air actually sampled, i.e., ug/m^3 . On this basis, a decision is made both on whether to calculate the quantity of each n-alkane equivalent present and on which analytical procedural pathway will be followed. If the total organic content is great enough to warrant continuing the analysis -- $>500 \text{ ug}/\text{m}^3$ -- a TCO of less than $75 \text{ ug}/\text{m}^3$ will require only LC fractionation and gravimetric determinations and IR spectra to be obtained on each fraction. If the TCO is greater than $75 \text{ ug}/\text{m}^3$, then the first seven LC fractions of each sample will be reanalyzed using this same gas chromatographic technique.

7.7 Calculations:

7.7.1 Boiling Point - Retention Time Calibration: The required data for this calibration are on the chromatogram and on the data sheet. The data reduction is performed as follows:

7.7.1.1 Average the retention times and calculate relative standard deviations for each n-hydrocarbon.

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7.7.1.2 Plot average retention times as abscissae versus normal boiling points as ordinates.

7.7.1.3 Draw in calibration curve.

7.7.1.4 Locate and record retention times corresponding to boiling ranges 90-100, 110-140, 140-160, 160-180, 180-200, 200-220, 220-240, 240-260, 260-280, 280-300°C.

7.7.2 Response-amount calibration: The required data for this calibration are on the chromatogram and on the data sheet. The data reduction is performed as follows:

7.7.2.1 Average the area responses of each standard and calculate relative standard deviations.

7.7.2.2 Plot response (uv·sec) as ordinate versus ng/uL as abscissa.

7.7.2.3 Draw in the curve. Perform least squares regression and obtain slope (uV·sec·uL/ng).

7.7.3 Total C7-C16 hydrocarbons analysis: The required data for this calculation are on the chromatogram and on the data sheet. The data reduction is performed as follows:

7.7.3.1 Sum the areas of all peaks within the retention time range of interest.

7.7.3.2 Convert this area (uV·sec) to ng/uL by dividing by the weight response for n-decane (uV·sec·uL/ng).

7.7.3.3 Multiply this weight by the total concentrate volume (10 mL) to get the weight of the C7-C16 hydrocarbons in the sample.

7.7.3.4 Using the volume of gas sampled or the total weight of sample acquired, convert the result of Step 7.7.3.3 above to ug/m³.

7.7.3.5 If the value of total C7-C16 hydrocarbons from Step 7.7.3.4 above exceeds 75 ug/m³, calculate individual hydrocarbon concentrations in accordance with the instructions in Paragraph 7.7.5.5 below.

7.7.4 Individual C7-C16 n-Alkane Equivalent Analysis: The required data from the analyses are on the chromatogram and on the data sheet. The data reduction is performed as follows:

7.7.4.1 Sum the areas of peaks in the proper retention time ranges.

7.7.4.2 Convert areas ($\mu\text{V}\cdot\text{sec}$) to $\text{ng}/\mu\text{L}$ by dividing by the proper weight response ($\mu\text{V}\cdot\text{sec}\cdot\mu\text{L}/\text{ng}$).

7.7.4.3 Multiply each weight by total concentrate volume (10 mL) to get weight of species in each range of the sample.

7.7.4.4 Using the volume of gas sampled on the total weight of sample acquired, convert the result of Step 7.7.4.3 above to $\mu\text{g}/\text{m}^3$.

8.0 QUALITY CONTROL

8.1 Appropriate QC is found in the pertinent procedures throughout the method.

9.0 METHOD PERFORMANCE

9.1 Even relatively comprehensive error propagation analysis is beyond the scope of this procedure. With reasonable care, peak area reproducibility of a standard should be of the order of 1% RSD. The relative standard deviation of the sum of all peaks in a fairly complex waste might be of the order of 5-10%. Accuracy is more difficult to assess. With good analytical technique, accuracy and precision should be of the order of 10-20%.

10.0 REFERENCES

1. Emissions Assessment of Conventional Stationary Combustion Systems: Methods and Procedure Manual for Sampling and Analysis, Interagency Energy/Environmental R&D Program, Industrial Environmental Research Laboratory, Research Triangle Park, NC 27711, EPA-600/7-79-029a, January 1979.

7.4 Adsorption Tube Procedure (Alternative Procedure). It is suggested that the tester refer to the National Institute of Occupational Safety and Health (NIOSH) method for the particular organics to be sampled. The principal interferent will be water vapor. If water vapor is present at concentrations above 3 percent, silica gel should be used in front of the charcoal. Where more than one compound is present in the emissions, then develop relative adsorptive capacity information.

7.4.1 Additional Apparatus. In addition to the equipment listed in the NIOSH method for the particular organic(s) to be sampled, the following items (or equivalent) are suggested.

7.4.1.1 Probe (Optional). Borosilicate glass or stainless steel, approximately 6-mm ID, with a heating system if water condensation is a problem, and a filter (either in-stack or out-stack heated to stack temperature) to remove particulate matter. In most instances, a plug of glass wool is a satisfactory filter.

7.4.1.2 Flexible Tubing. To connect probe to adsorption tubes. Use a material that exhibits minimal sample adsorption.

7.4.1.3 Leakless Sample Pump. Flow controlled, constant rate pump, with a set of limiting (sonic) orifices to provide pumping rates from approximately 10 to 100 cc/min.

7.4.1.4 Bubble-Tube Flowmeter. Volume accuracy within ± 1 percent, to calibrate pump.

7.4.1.5 Stopwatch. To time sampling and pump rate calibration.

7.4.1.6 Adsorption Tubes. Similar to ones specified by NIOSH, except the amounts of adsorbent per primary/backup sections are 800/200 mg for charcoal tubes and 1040/260 mg for silica gel tubes. As an alternative, the tubes may contain a porous polymer adsorbent such as Tenax GC or XAD-2.

7.4.1.7 Barometer. Accurate to 5 mm Hg, to measure atmospheric pressure during sampling and pump calibration.

7.4.1.8 Rotameter. 0 to 100 cc/min, to detect changes in flow rate during sampling.

7.4.2 Sampling and Analysis. It is suggested that the tester follow the sampling and analysis portion of the respective NIOSH method section entitled "Procedure." Calibrate the pump and limiting orifice flow rate through adsorption tubes with the bubble tube flowmeter before sampling. The sample system can be operated as a "recirculating loop" for this operation. Record the ambient temperature and barometric pressure. Then, during sampling, use the ro-

tameter to verify that the pump and orifice sampling rate remains constant.

Use a sample probe, if required, to obtain the sample at the centroid of the duct, or at a point no closer to the walls than 1 m. Minimize the length of flexible tubing between the probe and adsorption tubes. Several adsorption tubes can be connected in series, if the extra adsorptive capacity is needed. Provide the gas sample to the sample system at a pressure sufficient for the limiting orifice to function as a sonic orifice. Record the total time and sample flow rate (or the number of pump strokes), the barometric pressure, and ambient temperature. Obtain a total sample volume commensurate with the expected concentration(s) of the volatile organic(s) present, and recommended sample loading factors (weight sample per weight adsorption media). Laboratory tests prior to actual sampling may be necessary to predetermine this volume. When more than one organic is present in the emissions, then develop relative adsorptive capacity information. If water vapor is present in the sample at concentrations above 2 to 3 percent, the adsorptive capacity may be severely reduced. Operate the gas chromatograph according to the manufacturer's instructions. After establishing optimum conditions, verify and document these conditions during all operations. Analyze the audit samples (see Section 7.4.4.3), then the emission samples. Repeat the analysis of each sample until the relative deviation of two consecutive injections does not exceed 5 percent.

7.4.3 Standards and Calibration. The standards can be prepared according to the respective NIOSH method. Use a minimum of three different standards; select the concentrations to bracket the expected average sample concentration. Perform the calibration before and after each day's sample analyses. Prepare the calibration curve by using the least squares method.

7.4.4 Quality Assurance.

7.4.4.1 Determination of Desorption Efficiency. During the testing program, determine the desorption efficiency in the expected sample concentration range for each batch of adsorption media to be used. Use an internal standard. A minimum desorption efficiency of 50 percent shall be obtained. Repeat the desorption determination until the relative deviation of two consecutive determinations does not exceed 5 percent. Use the average desorption efficiency of these two consecutive determinations for the correction specified in Section 7.4.4.5. If the desorption efficiency of the compound(s) of interest is questionable under actual sampling conditions, use of the Method of Standard Additions may be helpful to determine this value.

7.4.4.2 Determination of Sample Collection Efficiency. For the source samples, ana-

lyze the primary and backup portions of the adsorption tubes separately. If the backup portion exceeds 10 percent of the total amount (primary and backup), repeat the sampling with a larger sampling portion.

7.4.4.3 Analysis Audit. Immediately before the sample analyses, analyze the two audits in accordance with Section 7.4.2. The analysis audit shall agree with the audit concentration within 10 percent.

7.4.4.4 Pump Leak Checks and Volume Flow Rate Checks. Perform both of these checks immediately after sampling with all sampling train components in place. Perform all leak checks according to the manufacturer's instructions, and record the results. Use the bubble-tube flowmeter to measure the pump volume flow rate with the orifice used in the test sampling, and the result. If it has changed by more than 5 but less than 20 percent, calculate an average flow rate for the test. If the flow rate has changed by more than 20 percent, recalibrate the pump and repeat the sampling.

7.4.4.5 Calculations. All calculations can be performed according to the respective NIOSH method. Correct all sample volumes to standard conditions. If a sample dilution system has been used, multiply the results by the appropriate dilution ratio. Correct all results by dividing by the desorption efficiency (decimal value). Report results as ppm by volume, dry basis.

7.5 Reporting of Results. At the completion of the field analysis portion of the study, ensure that the data sheets shown in Figure 18-11 have been completed. Summarize this data on the data sheets shown in Figure 18-15.

8. Bibliography

1. American Society for Testing and Materials. C, Through C, Hydrocarbons in the Atmosphere by Gas Chromatography. ASTM D 2820-72, Part 23. Philadelphia, Pa. 23:950-958. 1973.
2. Corazon, V. V. Methodology for Collecting and Analyzing Organic Air Pollutants. U.S. Environmental Protection Agency. Publication No. EPA-600/2-79-042. February 1979.
3. Dravnieks, A., B. K. Krotoszynski, J. Whitfield, A. O'Donnell, and T. Burgwald. Environmental Science and Technology. 5(12):1200-1222. 1971.
4. Eggertsen, F. T., and F. M. Nelsen. Gas Chromatographic Analysis of Engine Exhaust and Atmosphere. Analytical Chemistry. 30(6): 1040-1043. 1958.
5. Fearheller, W. R., P. J. Marn, D. H. Harris, and D. L. Harris. Technical Manual for Process Sampling Strategies for Organic Materials. U.S. Environmental Protection Agency. Research Triangle Park, NC. Publication No. EPA 600/2-76-122. April 1976. 172 p.

Sampling Equipment. Environmental Protection Agency. Research Triangle Park, N.C. APTD-0576. March, 1972.

4. Smith, W. S., R. T. Shigehara, and W. F. Todd. A Method of Interpreting Stack Sampling Data. Paper Presented at the 63rd Annual Meeting of the Air Pollution Control Association, St. Louis, Mo. June 14-19, 1970.

5. Smith, W. S., et al., Stack Gas Sampling Improved and Simplified with New Equipment. APCA Paper No. 67-119. 1967.

6. Specifications for Incinerator Testing at Federal Facilities. PHS, NCAPC. 1967.

7. Shigehara, R. T., Adjustments in the EPA Nomograph for Different Pitot Tube Coefficients and Dry Molecular Weights. Stack Sampling News 2:4-11. October, 1974.

8. Vollaro, R. F., A Survey of Commercially Available Instrumentation for the Measurement of Low-Range Gas Velocities. U.S. Environmental Protection Agency, Emission Measurement Branch. Research Triangle Park, N.C. November, 1976 (unpublished paper).

9. Annual Book of ASTM Standards. Part 28. Gaseous Fuels; Coal and Coke; Atmospheric Analysis. American Society for Testing and Materials. Philadelphia, Pa. 1974. pp. 617-622.

10. Vollaro, R. F., Recommended Procedure for Sample Traverses in Ducts Smaller than 12 Inches in Diameter. U.S. Environmental Protection Agency, Emission Measurement Branch. Research Triangle Park, N.C. November, 1976.

METHOD 18—MEASUREMENT OF GASEOUS ORGANIC COMPOUND EMISSIONS BY GAS CHROMATOGRAPHY

Introduction

This method should not be attempted by persons unfamiliar with the performance characteristics of gas chromatography, nor by those persons who are unfamiliar with source sampling. Particular care should be exercised in the area of safety concerning choice of equipment and operation in potentially explosive atmospheres.

1. Applicability and Principle

1.1 Applicability. This method applies to the analysis of approximately 90 percent of the total gaseous organics emitted from an industrial source. It does not include techniques to identify and measure trace amounts of organic compounds, such as those found in building air and fugitive emission sources.

This method will not determine compounds that (1) are polymeric (high molecular weight), (2) can polymerize before analysis, or (3) have very low vapor pressures at stack or instrument conditions.

1.2 Principle.

The major organic components of a gas mixture are separated by gas chromatography (GC) and individually quantified by flame ionization, photoionization, electron capture, or other appropriate detection principles.

The retention times of each separated component are compared with those of known compounds under identical conditions. Therefore, the analyst confirms the identity and approximate concentrations of the organic emission components beforehand. With this information, the analyst then prepares or purchases commercially available standard mixtures to calibrate the GC under conditions identical to those of the samples. The analyst also determines the need for sample dilution to avoid detector saturation, gas stream filtration to eliminate particulate matter, and prevention of moisture condensation.

2. Range and Sensitivity

2.1 Range. The range of this method is from about 1 part per million (ppm) to the upper limit governed by GC detector saturation or column overloading. The upper limit can be extended by diluting the stack gases with an inert gas or by using smaller gas sampling loops.

2.2 Sensitivity. The sensitivity limit for a compound is defined as the minimum detectable concentration of that compound, or the concentration that produces a signal-to-noise ratio of three to one. The minimum detectable concentration is determined during the presurvey calibration for each compound.

3. Precision and Accuracy

Gas chromatographic techniques typically provide a precision of 5 to 10 percent relative standard deviation (RSD), but an experienced GC operator with a reliable instrument can readily achieve 5 percent RSD. For this method, the following combined GC/operator values are required.

(a) Precision. Duplicate analyses are within 5 percent of their mean value.

(b) Accuracy. Analysis results of prepared audit samples are within 10 percent of preparation values.

4. Interferences

Resolution interferences that may occur can be eliminated by appropriate GC column and detector choice or by shifting the retention times through changes in the column flow rate and the use of temperature programming.

The analytical system is demonstrated to be essentially free from contaminants by periodically analyzing blanks that consist of hydrocarbon-free air or nitrogen.

Sample cross-contamination that occurs when high-level and low-level samples or standards are analyzed alternately, is best

APPENDIX L

CALCULATION EQUATIONS

METHOD 2
CALCULATION EQUATIONS

$$\bar{V}_s = 85.49 C_p (\sqrt{\Delta p})_{avg} \sqrt{\frac{T_{s(avg)}}{P_s M_s}}$$

$$Q_{s,d} = 60 (1 - B_{ws}) \bar{V}_s A \left(\frac{528}{T_{s(avg)}} \right) \left(\frac{P_s}{29.92} \right)$$

$$Q_a = 60 \bar{V}_s A$$

$$\dot{m}_s = \frac{4.995 Q_{s,d} G_d}{1 - B_{ws}}$$

$$RH^* = 100 (vp_{twb} - 0.0003641 P_s (T_{db} - T_{wb})) / vp_{tdb}$$

$$B_{ws}^* = RH(vp_{tdb}) / P_s$$

$$\rho = \frac{4.585 \times 10^{-2} P_s M_s}{T_s (avg)}$$

*Alternate equations for calculating moisture content from wet bulb and dry bulb data.

032294-G:\STACK\WPMETHODS-EQ.15

SYMBOLS

A	=	Cross Sectional area of stack, SQ. FT.
A_n	=	Cross sectional area of nozzle, SQ. FT.
B_{ws}	=	Water vapor in gas stream, proportion by volume
C_p	=	Pitot tube coefficient, dimensionless
C_1	=	Concentration of particulate matter in stack gas, wet basis, GR/ACF
C_s	=	Concentration of particulate matter in stack gas, dry basis, corrected to standard conditions, GR/DSCF
EA	=	Excess air, percent by volume
γ	=	Dry test meter correction factor, dimensionless
G_d	=	Specific gravity (relative to air), dimensionless
I	=	Isokinetic variation, percent by volume
M_d	=	Molecular weight of stack gas, dry basis, g/g - mole.
m_s	=	Mass flow of wet flue gas, LB/HR
m_p	=	Particulate mass flow, LB/HR
M_s	=	Molecular weight of stack gas, wet basis, g/g mole.
M_p	=	Total amount of particulate matter collected, g
P_{bar}	=	Atmospheric pressure, IN. HG. (uncompensated)
P_s	=	Stack static gas pressure, IN. WC.
P_s	=	Absolute pressure of stack gas, IN. HG.
P_{std}	=	Standard absolute pressure, 29.92 IN. HG.
A_s	=	Actual volumetric stack gas flow rate, ACFM
$Q_{s,d}$	=	Dry volumetric stack gas flow rate corrected to standard conditions, DSCFM
RH	=	Relative humidity, %

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T_{db}	=	Dry bulb temperature of stack gas, °F
T_{wb}	=	Wet bulb temperature of stack gas, °F
$T_{m(avg)}$	=	Absolute average dry gas meter temperature, °R
$T_{s(avg)}$	=	Absolute average stack temperature, °R
T_{std}	=	Standard absolute temperature, 528 °R (68 °F)
θ	=	Total sampling time, min.
V_{lc}	=	Total volume of liquid collected in impingers and silica gel, ml
V_m	=	Volume of gas sample as measured by dry gas meter, CF
$V_{m(std)}$	=	Volume of gas sample measured by the dry gas meter corrected to standard conditions, DSCF
$V_{w(std)}$	=	Volume of water vapor in the gas sample corrected to standard conditions, SCF
$\bar{V}_s$	=	Average actual stack gas velocity, FT/SEC
vp_{adb}	=	Vapor pressure at T_{db} , IN. HG.
vp_{twb}	=	Vapor pressure at T_{wb} , IN. HG.
$\overline{\Delta H}$	=	Average pressure differential across the orifice meter, IN. WC.
ΔP	=	Velocity pressure of stack gas, IN. WC.
γ	=	Dry test meter correction coefficient, dimensionless
ρ	=	Actual gas density, LB/ACF

METHOD 3
CALCULATION EQUATIONS

$$\%EA = \frac{100(\%O_2 - 0.5\% CO)}{0.264\% N_2 - \%O_2 + 0.5\% CO}$$

$$M_d = 0.44(\%CO_2) + 0.32 (\%O_2) + 0.28 (\%N_2 + \%CO)$$

$$M_s = M_d (I - B_{ws}) + 0.18 B_{ws}$$

$$B_{ws} = \frac{V_{w(std)}}{V_{w(std)} + V_{m(std)}}$$

METHOD 5
CALCULATION EQUATIONS

$$V_{m(std)} = 17.65 V_m \gamma \left(\frac{P_{bar} + \overline{\Delta H}/13.6}{T_{m(avg)}} \right)$$

$$V_{w(std)} = 0.0472 V_{ls}$$

$$B_{ws} = \frac{V_{w(std)}}{V_{w(std)} + V_{m(std)}}$$

$$I = 0.0944 \left(\frac{T_{s(avg)} V_{m(std)}}{P_s V_s A_n \theta (I - B_{ws})} \right)$$

$$C_s = \frac{15.43 M_p}{V_{m(std)}}$$

$$C_a = \frac{272.3 M_p P_s}{T_{s(avg)} (V_{w(std)} + V_{m(std)})}$$

$$(\dot{m}_p)_1 = 8.5714 \times 10^{-3} C_s Q_{s,d}$$

$$(\dot{m}_p)_2 = \frac{1.3228 \times 10^{-1} M_p A}{\theta A_n}$$

$$\dot{m}_p = \frac{(\dot{m}_p)_1 + (\dot{m}_p)_2}{2}$$

CALCULATION EQUATIONS

METHOD 7

$$V_{m(std)} = 17.64 (V_f - 25) \left[\frac{P_f}{T_f} - \frac{P_i}{T_i} \right]$$

$$C_s = 6.243 \times 10^{-5} \frac{M}{V_{m(std)}}$$

$$E = \frac{2090 C_s F}{20.9 - \bar{B}'_{O_2}}$$

$$C_s (GR/DSCF) = 7000 C_s$$

$$C_s (MG/DSCM) = 1.60186 \times 10^7 C_s$$

$$C_s (ppm-dry) = 8.37552 \times 10^6 C_s$$

$$C_s (ppm-3\% O_2) = 8.37552 \times 10^6 C_s \left(1 + \left[\frac{\bar{B}'_{O_2} - 3}{20.9 - \bar{B}'_{O_2}} \right] \right)$$

$$C_s (ppm-wet) = 8.37552 \times 10^6 C_s \left(1 - \frac{MC}{100} \right)$$

SYMBOLS

$\bar{B} O_2$	=	Average oxygen content in flue gas, % v/v
C_s	=	Concentration of nitrogen oxides in flue gas, dry basis, corrected to standard conditions, LB/DSCF
C_s (GR/DSCF)	=	Concentration of nitrogen oxides in flue gas, dry basis, corrected to standard conditions, GR/DSCF
C_s (MG/DSCM)	=	Concentration of nitrogen oxides in flue gas, dry basis, corrected to standard conditions, MG/DSCM
E	=	Emission factor, LB/10 ⁶ BTU
F	=	F-Factor for given fuel type, DSCF/10 ⁶ BTU
M	=	Mass of nitrogen oxides as nitrogen dioxide in gas sample, ug
MC	=	Moisture content of flue gas, %
P_f	=	Final absolute pressure in flask, IN. HG
P_i	=	Initial absolute pressure in flask, IN. HG
C_s (ppm-dry)	=	Concentration of nitrogen oxides in flue gas, dry basis, (v/v), ppm
C_s (ppm-3% O ₂)	=	Concentration of nitrogen oxides in flue gas, dry basis, corrected to 3% O ₂ , (v/v) ppm
C_s (ppm-wet)	=	Concentration of nitrogen oxides in flue gas, wet basis, (v/v), ppm
T_f	=	Final absolute temperature in flask, °R
T_i	=	Initial absolute temperature in flask, °R
V_f	=	Volume of flask and valve, cc
$V_{m(std)}$	=	Sample volume at standard conditions, dry basis, cc

CALCULATION EQUATIONS

METHOD 10

$$CO\text{-}PPM\text{-}DRY = CO_{CO_2} - \text{free, dry, avg} (1 - CO_2, d/100)$$

$$CO\text{-}PPM\text{-}WET = CO\text{-}PPM\text{-}DRY (1 - MC/100)$$

$$GR/DSCF = 5.0885 \times 10^{-4} (CO\text{-}PPM\text{-}DRY)$$

$$mg/dscm = 1.165 (CO\text{-}PPM\text{-}DRY)$$

$$\dot{m} = 8.5714 \times 10^{-3} (GR/DSCF) (Q_{s,d})$$

$$E = \frac{2.9857 \times 10^{-3} F_d (GR/DSCF)}{20.9 - O_{2,d}}$$

where:

$CO_{CO_2} - \text{free, dry, avg}$

= average of two determinations of carbon monoxide on a dry, CO_2 - free integrated flue gas sample reported in ppm by volume

$CO_{2,d}$ = carbon dioxide concentration of flue gas on a dry percent by volume basis

$O_{2,d}$ = oxygen concentration of flue gas on a dry percent by volume basis

MC	=	moisture content of flue gas on a percent by volume basis
CO-PPM-DRY	=	carbon monoxide concentration in ppm by volume on a dry basis
CO-PPM-WET	=	carbon monoxide concentration in ppm by volume on a wet or actual basis
GR/DSCF	=	concentration of carbon monoxide in flue gas on a grains per dry standard cubic foot basis (68 °F, 29.92 IN. HG.)
mg/dscm	=	concentration of carbon monoxide in flue gas on a milligrams per dry standard cubic meter basis (60 °F, 29.92 IN. HG.)
m	=	emissions or mass rate of carbon monoxide on a LB/HR basis
Q_d	=	volumetric flow rate of flue gas in dry standard cubic feet per minute
E	=	emission factor of carbon monoxide in pounds of carbon monoxide emitted per million BTU heat input (LB/MMBTU)
F_d	=	F-Factor of respective fuel in dry standard cubic feet of exhaust gas at 0% oxygen per million BTU of heat input (DSCF/MMBTU)

METHOD 25A

Total Gaseous Organics Calculation Equation

$$\text{GR C/SCF} = 2.180 \times 10^{-4} (\text{ppm, w})$$

$$\text{GR C/DSCF} = 2.180 \times 10^{-4} (\text{ppm, w}) / (1 - \text{MC}/100)$$

$$\text{LB C/HR} = 8.5714 \times 10^{-3} (\text{GR/DSCF}) (\text{DSCFM})$$

where:

GR C/SCF = grains of total gaseous organics as carbon per actual (wet) standard cubic foot

GR C/DSCF = grains of total gaseous organics as carbon per dry standard cubic foot

LB C/HR = pounds of total gaseous organics as carbon emitted per hour

Note 1: The Ratfisch Model RS 55 Heated FID Analyzer as normally operated with a heated filter, sample line and heated detector oven gives ppm, w.

Note 2: ppm, C = ppm as carbon = 3(ppm propane)

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CALCULATION EQUATIONS

Gas Chromatographic Method for Phenol in Air

$$\text{PPM-DRY} = \frac{9.03 \times 10^{-3} m}{V_{\text{std}}}$$

$$\text{PP-WET} = \text{PPM-DRY} (1 - \text{MC}/100)$$

$$\text{GR/DSCF} = 1.709 \times 10^{-3} (\text{PPM-DRY})$$

$$\text{mg/dscm} = 3.913 (\text{PPM-DRY})$$

$$m = 8.5714 \times 10^{-3} (\text{GR/DSCF}) (Q_{\text{std}})$$

where:

PPM-DRY = concentration of phenol in gas in parts per million by volume on a dry basis

PPM-WET = concentration of phenol in gas in parts per million by volume on an actual or wet basis

MC = moisture content of gas on a percent by volume basis

GR/DSCF = concentration of phenol in gas on a grains per dry standard cubic foot basis (68 °F, 29.92 IN. HG.)

m = emission or mass rate of phenol in pounds per hour (LB/HR)

Q_{std} = volumetric flow rate of stack gas in dry standard cubic feet per minute (DSCFM)

030994-G:\STACK\WPMETHODS\IS-EQ.01

CALCULATION EQUATIONS

Chromotropic Acid Method for Formaldehyde

$$m_t = \frac{m_a V_{soln}}{V_{aliq}}$$

where:

m_t	=	mass of formaldehyde in total sample in ug
m_a	=	mass of formaldehyde in aliquot in ug
V_{soln}	=	volume of total sample in cc (500 cc normally)
V_{aliq}	=	volume of aliquot taken for analysis in cc
PPM·DRY	=	$\frac{0.0283 m_t}{V_{std}}$
PPM·WET	=	PPM·DRY (1-MC/100)
GR/DSCF	=	5.45×10^{-4} (PPM·DRY)
mg/dscm	=	1.249 (PPM·DRY)
$\dot{m}$	=	8.5714×10^{-3} (GR/DSCF) ($Q_{\dot{v}}$)

where:

PPM·DRY	=	concentration of formaldehyde in parts per million by volume on a dry basis
PPM·WET	=	concentration of formaldehyde in parts per million by volume on an actual or wet basis
MC	=	moisture content of gas on a percent by volume basis
GR/DSCF	=	concentration of formaldehyde in gas on a grains per dry standard cubic foot basis (68 °F, 29.92 IN. HG.)
$\dot{m}$	=	emission or mass rate of formaldehyde in pounds per hour (LB/HR)
V_{std}	=	dry gas volume as measured by the dry gas meter, corrected to standard conditions (at 68 °F and 1 atmosphere) DSCF

031894-G:\STACK\WPMETHODS-EQ.03

Concentration Calculation Equations for Benzene

1. Structure:  C_6H_6	2. Molecular weight: <u>78.11</u> g/g-mole
3. Mass/volume Concentration: $C_{ug/Nm^3} = \frac{35.314 \text{ m}}{V_{std}}$ where m = Total mass of <u>Benzene</u> in sample in micrograms (ug), and Vstd = Total volume of exhaust gas or air sampled in dry standard cubic feet (DSCF).	
4. Volume/volume Concentration: $C_{ppmv}^{C_6H_6} = \left(\frac{mg}{Nm^3} \right) \times \left(\frac{24,054 \text{ mL}}{78.11 \text{ mg}} \right) = ppmv$ $C_{ppmv}^{C_6H_6} = 0.3080 \left(\frac{C_{ug/Nm^3}^{C_6H_6}}{C_{ug/Nm^3}} \right)$	
5. Notes:	
Derived by: <u>D. DESPEN</u>	Date: <u>9-10-90</u>

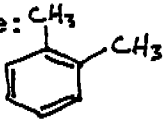
INTERPOLL LABORATORIES, INC

Concentration Calculation Equations for TOLUENE

1. Structure:  C_7H_8	2. Molecular weight: <u>92.14</u> g/g-mole
3. Mass/volume Concentration: $C_{ug/Nm^3} = \frac{35.314 \text{ m}}{V_{std}}$ where $\frac{m}{R_d} =$ Total mass of <u>toluene</u> in sample in micrograms (ug), and $V_{std} =$ Total volume of exhaust gas or air sampled in dry standard cubic feet (DSCF). $R_d =$ Percent by weight recovery of toluene by solvent desorption from charcoal.	
4. Volume/volume Concentration: $\frac{C_7H_8}{C_{ppmv}} = \frac{24.054 \text{ mL}}{92.14 \text{ mg}} \cdot \frac{\mu g}{Nm^3}$ $\frac{C_7H_8}{C_{ppmv}} = 0.2611 \cdot C_{ug/Nm^3}$	
5. Notes:	
Derived by: <u>P.L.</u>	Date: <u>5-7-90</u>

INTERPOLL LABORATORIES, INC

Concentration Calculation Equations for XYLENE(S)

1. Structure:  C_8H_{10}	2. Molecular weight: <u>106.17</u> g/g-mole
3. Mass/volume Concentration: $C_{ug/Nm^3} = \frac{35.314 \text{ m}}{V_{std}}$ where $\frac{m}{R_d} =$ Total mass of <u>xylene(s)</u> in sample in micrograms (ug), and $V_{std} =$ Total volume of exhaust gas or air sampled in dry standard cubic feet (DSCF). $R_d =$ Percent by weight recovery of n-butanol by solvent desorption from charcoal.	
4. Volume/volume Concentration: $\frac{C_8H_{10}}{C_{ppmv}} = \frac{\mu g}{Nm^3} \cdot \frac{24.054 \text{ ml}}{106.17 \text{ mg}}$ $\frac{C_8H_{10}}{C_{ppmv}} = 0.2266 \cdot C_{ug/Nm^3}$	
5. Notes:	
Derived by: <u>P.L.</u>	Date: <u>5-7-90</u>

LP - Hayward				
			Report No. 4-3097	
OXIDES OF NITROGEN				
LB/HR CALCULATIONS				
Line 1 Press RTO Stack				
RUN	NOx ppm	Flow	LB/DSCF	LB/HR
1	25	68420	2.98E-06	12.25361
2	16.8	65960	2.01E-06	7.93836
3	14.5	66160	1.73E-06	6.872335
Line 2 Press RTO Stack				
RUN	NOx ppm	Flow	LB/DSCF	LB/HR
1	14.2	81740	1.7E-06	8.31503
2	12	80990	1.43E-06	6.962312
3	8.4	79770	1E-06	4.800204
CARBON MONOXIDE				
LB/HR CALCULATIONS				
Line 1 Press RTO Stack				
RUN	CO ppm	Flow	LB/DSCF	LB/HR
1	17.2	68420	1.25E-06	5.130482
2	9.7	65960	7.05E-07	2.789324
3	8.7	66160	6.32E-07	2.509351
Line 2 Press RTO Stack				
RUN	CO ppm	Flow	LB/DSCF	LB/HR
1	9	81740	6.54E-07	3.207183
2	12.6	80990	9.16E-07	4.448858
3	11.5	79770	8.36E-07	3.999301

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		LP - HAYWARD			Report No. 4-3097	
		Hayward, Wisconsin				
		EMISSION FACTOR CALCULATIONS				
		(F-Factor Method)				
Line 1 Konus Stack		NOx			Emission	
		F-Factor		Concentr	Oxygen	Factor
	Run #	DSCF/MMBTU	M	(ppm,d)	(%v/v,d)	LB/MMBTU
	1	9600	46.01	78	14.5	0.2920
	2	9600	46.01	80	15.5	0.3549
	3	9600	46.01	70	13.5	0.2266
	AVG			76		0.2912
Line 2 Konus Stack					Emission	
		F-Factor		Concentr	Oxygen	Factor
	Run #	DSCF/MMBTU	M	(ppm,d)	(%v/v,d)	LB/MMBTU
	1	9600	46.01	57	16.4	0.3035
	2	9600	46.01	58	16.5	0.3158
	3	9600	46.01	73	15.9	0.3498
	AVG			62.667		0.3230
Line 1 Konus Stack		CO			Emission	
		F-Factor		Concentr	Oxygen	Factor
6/8/94	Run #	DSCF/MMBTU	M	(ppm,d)	(%v/v,d)	LB/MMBTU
1538-1640	1	9600	28	92	14.5	0.2096
1708-1811	2	9600	28	90	15.5	0.2430
1835-1935	3	9600	28	704	13.5	1.3870
	AVG			295.33		0.6132
6/9/94						
1345-1606	1	9600	28	61	14.5	0.1390
1632-1743	2	9600	28	179	13.5	0.3527
1802-1904	3	9600	28	53	14.2	0.1153
	AVG			97.667		0.2023
0851-1052	1	9600	28	105	15.4	0.2783
1240-1534	2	9600	28	104	14.9	0.2527
1610-1812	3	9600	28	135	13.8	0.2772
	AVG			114.67		0.2694
Line 2 Konus Stack					Emission	
		F-Factor		Concentr	Oxygen	Factor
	Run #	DSCF/MMBTU	M	(ppm,d)	(%v/v,d)	LB/MMBTU
	1	9600	28	73	16.4	0.2365
	2	9600	28	67	16.5	0.2220
	3	9600	28	62	15.9	0.1808
	AVG			67.333		0.2131

							Report No. 4-3097
				LP - Hayward			
				Hayward, Wisconsin			
Line 1 Press RTO Stack				MDI CALCULATIONS			
6/8/94							
	TIME	Vstd		Mass	Flow	Conc	Conc Mass Rate
RUN #	(HRS)	(DSCF)		(ug)	DSCFM	(mg/Nm3)	ppm (LB/HR)
1	0815-0916	36.45		5.2	68445	0.00504	0.000484 0.001292
2	0945-1046	36.62	<	2.5	68680	0.00241	0.000232 0.00062
3	1115-1216	37.05		5.4	69700	0.00515	0.000495 0.001344
Avg							0.000403 0.001085
Line 2 Press RTO Stack							
6/9/94							
	TIME	Vstd		Mass	Flow	Conc	Conc Mass Rate
RUN #	(HRS)	(DSCF)		(ug)	DSCFM	(mg/Nm3)	ppm (LB/HR)
1	1325-1440	56.78		12.2	79900	0.00759	0.000729 0.002271
2	1518-1641	34.34	<	2.5	77760	0.00257	0.000247 0.000749
3	1712-1828	36.12		6.5	81990	0.00635	0.000611 0.001952
Avg							0.000529 0.001657

APPENDIX M

SAMPLING TRAIN CALIBRATION DATA

INTERPOLL LABORATORIES
EPA Method 5 Gas Metering System
Quality Control Check Data Sheet

Job L.P. Hayward
 Operator DHS

Date 6/10/91
 Module No. 6

Instructions: Operate the control module at a flow rate equal to ΔH_e for 10 minutes before attaching the umbilical. Record the following data:

Bar press 28.76 in. Hg. $\tau =$.9947 ΔH_e 1.97 in. W.C.

Time (min)	Volume (CF)	Meter Temp. (°F)	
		Inlet	Outlet
	(892.60)		
2.5	894.49	66	63
5.0	896.40	70	63
7.5	898.39	74	64
10	900.29	77	64
	$V_m = 7.69$	$Avg(t_m) = 67.62$ °F	

Calculate Y_{cn} as follows:

$$Y_{cn} = \frac{1.786}{\tau V_m} \left[\frac{(t_m + 460)}{P_b} \right]^{0.5}$$

$$Y_{cn} = \frac{1.786}{(.9947)(7.69)} \left[\frac{(67.62) + 460}{(28.76)} \right]^{0.5}$$

$$Y_{cn} = \underline{1.0000}$$

If Y_{cn} is not within the range of 0.97 to 1.03, "the volume metering system should be investigated before beginning."

CFR Title 40, Part 60, Appendix A, Method 5, Section 4.4.1

S-432

EPA Method 5 Gas Metering System
Quality Control Check Data Sheet

Job L.P. / Hayward, WI

Date 6-10-94

Operator M. Kachler

Module No. 9

Instructions: Operate the control module at a flow rate equal to ΔH_0 for 10 minutes before attaching the umbilical. Record the following data:

Bar press 28.93 in. Hg. $\tau =$.9961 ΔH_0 1.78 in. W.C.

Time (min)	Volume (CF)	Meter Temp. (°F)	
		Inlet	Outlet
	(954.00)		
2.5	955.94	61	60
5.0	957.89	62	60
7.5	959.84	65	61
10	961.78	67	61
	$V_m = 7.78$	Avg (t_m) = 62.13 °F	

Calculate Y_{en} as follows:

$$Y_{en} = \frac{1.786}{\tau V_m} \left[\frac{(t_m + 460)}{P_b} \right]^{0.5}$$

$$Y_{en} = \frac{1.786}{(.9961)(7.78)} \left[\frac{(62.13) + 460}{(28.93)} \right]^{0.5}$$

$$Y_{en} = \underline{.979}$$

If Y_{en} is not within the range of 0.97 to 1.03, "the volume metering system should be investigated before beginning."

CFR Title 40, Part 60, Appendix A, Method 5, Section 4.4.1

S-432R

INTERPOLL LABORATORIES
EPA Method 5 Gas Metering System
Quality Control Check Data Sheet

Job L.P. / Hayward, Ill

Date 6-9-94

Operator M. Kachler

Module No. 9

Instructions: Operate the control module at a flow rate equal to ΔH_0 for 10 minutes before attaching the umbilical. Record the following data:

Bar press 29.90 in. Hg. $\tau =$ 9961 ΔH_0 1.78 in. W.C.

Time (min)	Volume (CF)	Meter Temp. (°F)	
		Inlet	Outlet
	(668.90)		
2.5	670.92	56	55
5.0	672.78	57	56
7.5	674.68	59	56
10	676.62	60	57
	$V_m = 7.72$	$Avg(t_m) = 57.00$ °F	

Calculate Y_{cn} as follows:

$$Y_{cn} = \frac{1.786}{\tau V_m} \left[\frac{(t_m + 460)}{P_b} \right]^{0.5}$$

$$Y_{cn} = \frac{1.786}{(9961)(7.72)} \left[\frac{(57.00) + 460}{(29.90)} \right]^{0.5}$$

$$Y_{cn} = \underline{.982}$$

If Y_{cn} is not within the range of 0.97 to 1.03, "the volume metering system should be investigated before beginning."

CFR Title 40, Part 60, Appendix A, Method 5, Section 4.4.1

S-432

INTERPOLL LABORATORIES
EPA Method 5 Gas Metering System
Quality Control Check Data Sheet

Job L.P. / Hayward, WI

Date 6-8-94

Operator M. Kautler

Module No. 9

Instructions: Operate the control module at a flow rate equal to ΔH_0 for 10 minutes before attaching the umbilical. Record the following data:

Bar press 28.98 in. Hg. $\tau =$.9961 ΔH_0 1.78 in. W.C.

Time (min)	Volume (CF)	Meter Temp. (°F)	
		Inlet	Outlet
	(343.40)		
2.5	345.35	48	48
5.0	347.25	49	48
7.5	349.16	50	49
10	351.09	52	49
	$V_m = 2.69$	$Avg(t_m) = 49.125^\circ F$	

Calculate Y_{cn} as follows:

$$Y_{cn} = \frac{1.786}{\tau V_m} \left[\frac{(t_m + 460)}{P_b} \right]^{0.5}$$

$$Y_{cn} = \frac{1.786}{(.9961)(2.69)} \left[\frac{(49.125) + 460}{(28.98)} \right]^{0.5}$$

$$Y_{cn} = \underline{.977}$$

If Y_{cn} is not within the range of 0.97 to 1.03, "the volume metering system should be investigated before beginning."

CFR Title 40, Part 60, Appendix A, Method 5, Section 4.4.1

S-432

EPA Method 5 Gas Metering System
Quality Control Check Data Sheet

Job L.P. / Hayward, WI

Date 6-8-94

Operator M. Kaehler

Module No. 10

Instructions: Operate the control module at a flow rate equal to ΔH for 10 minutes before attaching the umbilical. Record the following data:

Bar press 28.98 in. Hg. $\tau =$.9930 ΔH 1.77 in. W.C.

Time (min)	Volume (CF)	Meter Temp. ($^{\circ}$ F)	
		Inlet	Outlet
	(571.00)		
2.5	572.90	71	67
5.0	574.80	73	67
7.5	576.69	76	68
10	578.58	79	68
	$V_m = 7.58$	Avg (t_m) = 47.42 $^{\circ}$ F	

Calculate Y_{en} as follows:

$$Y_{en} = \frac{1.786}{\tau V_m} \left[\frac{(t_m + 460)}{P_b} \right]^{0.5}$$

$$Y_{en} = \frac{1.786}{(.9930)(7.58)} \left[\frac{(47.42) + 460}{(28.98)} \right]^{0.5}$$

$$Y_{en} = \underline{.993}$$

If Y_{en} is not within the range of 0.97 to 1.03, "the volume metering system should be investigated before beginning."

CFR Title 40, Part 60, Appendix A, Method 5, Section 4.4.1

S-432R

INTERPOLL LABORATORIES
EPA Method 5 Gas Metering System
Quality Control Check Data Sheet

Job LP - HAWAII
 Operator SLB

Date 6-7-94
 Module No. 14

Instructions: Operate the control module at a flow rate equal to ΔH for 10 minutes before attaching the umbilical. Record the following data:

Bar press 28.59 in. Hg. $\tau =$ 1.0066 ΔH 1.85 in. W.C.

Time (min)	Volume (CF)	Meter Temp. (°F)	
		Inlet	Outlet
<u>2.5</u>	<u>532.94</u>	<u>78</u>	<u>77</u>
<u>5.0</u>	<u>534.84</u>	<u>79</u>	<u>76</u>
<u>7.5</u>	<u>536.75</u>	<u>81</u>	<u>76</u>
<u>10</u>	<u>538.74</u>	<u>83</u>	<u>77</u>
	$V_m = 7.74$	$Avg(t_m) = 77.58$ °F	

Calculate Y_{cn} as follows:

$$Y_{cn} = \frac{1.786}{\tau V_m} \left[\frac{(t_m + 460)}{P_b} \right]^{0.5}$$

$$Y_{cn} = \frac{1.786}{(1.0066)(7.74)} \left[\frac{(78.34) + 460}{28.59} \right]^{0.5}$$

$$Y_{cn} = \underline{0.9948}$$

If Y_{cn} is not within the range of 0.97 to 1.03, "the volume metering system should be investigated before beginning."

CFR Title 40, Part 60, Appendix A, Method 5, Section 4.4.1

S-432

INTERPOLL LABORATORIES
EPA Method 5 Gas Metering System
Quality Control Check Data Sheet

Job A.P. / Hayward, W.

Date 6-7-94

Operator M. Kachler

Module No. _____

Instructions: Operate the control module at a flow rate equal to ΔH for 10 minutes before attaching the umbilical. Record the following data:

Bar press 28.73 in. Hg. $T =$ 9961 ΔH 1.78 in. W.C.

Time (min)	Volume (CF)	Meter Temp. (°F)	
		Inlet	Outlet
	(990.30)		
2.5	992.23	64	64
5.0	994.15	65	64
7.5	996.10	68	64
10	999.02	69	64
	$V_m = 7.72$	$Avg(t_m) = 65.25^\circ F$	

Calculate Y_{cn} as follows:

$$Y_{cn} = \frac{1.786}{T \cdot V_m} \left[\frac{(t_m + 460)}{P_b} \right]^{0.5}$$

$$Y_{cn} = \frac{1.786}{(9961)(7.72)} \left[\frac{(65.25) + 460}{(28.73)} \right]^{0.5}$$

$$Y_{cn} = \underline{.993}$$

If Y_{cn} is not within the range of 0.97 to 1.03, "the volume metering system should be investigated before beginning."

CFR Title 40, Part 60, Appendix A, Method 5, Section 4.4.1

S-432

Interpoll Laboratories, Inc.
(612) 786-6020

Meter Box Calibration and Usage Status

Date of Report: July 20, 1994

Meter Box No. : 2 (Rockwell Dry Test Meter Serial No. 964551)

Date of Last Calibration: March 24, 1994
Calibration Technician: E. Trowbridge
Wet Test Meter No.: American Meter AL-20

Date of Use	Report No.	Initial Meter		Final Meter		Volume/Job (cu. ft.)	Total Volume* (cu. ft.)
		Reading		Reading			
March 30, 1994	4-2559	994.50		1149.99		155.49	155.49
April 6, 1994	4-2598	1160.80		1592.09		431.29	586.78
June 8, 1994	4-3097	1781.90		2184.95		403.05	989.83

* Total volume + balance

* Total volume through meter since last calibration.

Interpoll Laboratories, Inc.
(612) 786-6020

Meter Box Calibration and Usage Status

Date of Report: July 20, 1994

Meter Box No. : 3 (Rockwell Dry Test Meter Serial No. 949231)

Date of Last Calibration: April 21, 1994

Calibration Technician: E. Trowbridge

Wet Test Meter No.: American Meter AL-20

Date of Use	Report No.	Initial Meter		Final Meter		Volume/Job (cu. ft.)	Total Volume* (cu. ft.)
		Reading		Reading			
April 26, 1994	4-2738	322.70		421.10		98.4	98.4
May 24, 1994	4-2971	458.20		933.28		475.08	573.48
June 02, 1994	4-3022	941.81		1216.25		274.44	847.92
June 09, 1994	4-3097	1216.62		1354.67		138.05	985.97

* Total volume through meter since last calibration.

Interpoll Laboratories, Inc.
(612) 786-6020

Meter Box Calibration and Usage Status

Date of Report: July 21, 1994

Meter Box No. : 6 (Rockwell Dry Test Meter Serial No. 964548)

Date of Last Calibration: May 31, 1994

Calibration Technician: E. Trowbridge

Wet Test Meter No.: American Meter AL-20

Date of Use	Report No.	Initial Meter Reading	Final Meter Reading	Volume/Job (cu. ft.)	Total Volume* (cu. ft.)
June 08, 1994	4-3097	394.96	1054.55	659.59	659.59

* Total volume through meter since last calibration.

Interpoll Laboratories, Inc.
(612) 786-6020

Meter Box Calibration and Usage Status

Date of Report: July 21, 1994

Meter Box No. : 9 (Rockwell Dry Test Meter Serial No. 964549)

Date of Last Calibration: March 24, 1994

Calibration Technician: E. Trowbridge

Wet Test Meter No.: American Meter AL-20

Date of Use	Report No.	Initial Meter Reading	Final Meter Reading	Volume/Job (cu. ft.)	Total Volume* (cu. ft.)
April 06, 1994	4-2597	261.00	391.84	130.84	130.84
April 12, 1994	4-2649	400.30	612.20	211.90	342.74
May 10, 1994	4-2837	624.20	1606.81	982.61	1325.35
May 17, 1994	4-2893	1615.60	1826.77	211.17	1536.52
June 02, 1994	4-3068	1842.90	1989.75	146.85	1683.37
June 09, 1994	4-3097	1998.20	3111.64	1113.44	2796.81

* Total volume through meter since last calibration.

Interpoll Laboratories, Inc.
(612) 786-6020

Meter Box Calibration and Usage Status

Date of Report: July 20, 1994

Meter Box No. : 14 (Rockwell Dry Test Meter Serial No. 1334119)

Date of Last Calibration: April 25, 1994

Calibration Technician: E. Trowbridge

Wet Test Meter No.: American Meter AL-20

Date of Use	Report No.	Initial Meter Reading	Final Meter Reading	Volume/Job (cu. ft.)	Total Volume* (cu. ft.)
April 29, 1994	4-2743	373.45	477.56	104.11	104.11
May 03, 1994	4-2801	486.40	703.12	216.72	320.83
May 05, 1994	4-2800	711.35	953.51	242.16	562.99
May 24, 1994	4-2971	953.75	1291.90	338.15	901.14
June 01, 1994	4-3026	1301.15	1530.75	229.60	1130.74
June 07, 1994	4-3097	1538.90	2301.98	763.08	1893.82

* Total volume through meter since last calibration.

Interpoll Laboratories, Inc.
(612) 786-6020

Meter Box Calibration and Usage Status

Date of Report: July 20, 1994

Meter Box No. : 10 (Rockwell Dry Test Meter Serial No. 1334112)

Date of Last Calibration: May 31, 1994

Calibration Technician: E. Trowbridge

Test Meter No.: American Meter AL-20

Date of Use	Report No.	Initial Meter Reading	Final Meter Reading	Volume/Job (cu. ft.)	Total Volume* (cu. ft.)
June 01, 1994	4-3020	104.50	570.30	465.80	465.80
June 09, 1994	4-3097	578.60	717.65	139.05	604.85

* Total volume through meter since last calibration.

Interpoll Laboratories, Inc.
(612) 786-6020

Meter Box Calibration and Usage Status

Date of Report: July 20, 1994

Meter Box No. : 2-S (Rockwell Dry Test Meter Serial No. 69185)

Date of Last Calibration: January 13, 1994

Calibration Technician: S. Bainville

Wet Test Meter No.: American Meter AL-17 (0.05 CF/REV)

Date of Use	Report No.	Initial Meter		Final Meter		Volume/Job (cu. ft.)	Total Volume* (cu. ft.)
		Reading		Reading			
January 20, 1994	4-2118	396.000		398.532		2.532	2.532
March 04, 1994	4-2384	406.300		433.333		27.033	29.565
May 11, 1994	4-2839	434.450		436.850		2.400	31.965
June 09, 1994	4-3097	436.910		443.688		6.778	38.743

* Total volume through meter since last calibration.

Interpoll Laboratories, Inc.
(612) 786-6020

Meter Box Calibration and Usage Status

Date of Report: July 25, 1994

Meter Box No.: 5-S (Rockwell Dry Test Meter Serial No. 64711)
Date of Last Calibration: January 21, 1994
Calibration Technician: S. Bainville

Wet Test Meter No.: American Meter AL-17 (0.05 CF/REV)

Date of Use	Report No.	Initial Meter Reading	Final Meter Reading	Volume/Job (cu. ft.)	Total Volume* (cu. ft.)
March 08, 1994	4-2410	905.624	911.374	5.750	5.750
March 22, 1994	4-2518	911.400	915.157	3.757	9.507
April 12, 1994	4-2117	915.426	921.422	5.996	15.503
June 07, 1994	4-3097	921.500	929.139	7.639	23.142

* Total volume through meter since last calibration.

Date 3-24-94
Bar. Press. 29.00 in. Hg.

INTERPOLL LABORATORIES, INC.
METER CALIBRATION SHEET
EPA METHOD 5

Technician St. Paul

[illegible]

Positive leak check performed by
 Water was in tolerance ☒
 Water was not in tolerance ☐; readjusted linkage
 Water was not in tolerance ☐; changed dry test meters

Approved by Ranish K. exp. Date 7/4/94

* Based on AL-20 wet test meter calibration in Nov. 1991 against Bell Prover (NBS Traceable) - Carl Poe Co.

S0102RR 11/91

Control Module No.
Serial No. DIN 444231
Net Test Meter No. AL-20
Technician SS [Signature]

AL-20

Technician E. J. J. J. J. J.

[illegible]

Positive leak check performed by
 Water was in tolerance ☒
 Water was not in tolerance ☐; readjusted linkage
 Water was not in tolerance ☐; changed dry test meters

Approved by Hubert H. K. Date 4/27/94

Bar. Press. 29.12 in. Hg

INTERPOLL LABORATORIES, INC.
METER CALIBRATION SHEET

9 DOMESTIC VIOLENCE

Control Module No.

Serial No. DIN

Wat Test Water No.

Technician

[illegible]

Positive leak check performed by
 Meter was in tolerance ☒
 Meter was not in tolerance ☐; readjusted linkage
 Meter was not in tolerance ☐; changed dry test meters

Approved by Dan Smith Date 6/6/99

* Based on AL-20 wet test meter calibration in Nov. 1991 against Bell Prover (NDS Traceable) - Carl Poe Co.

50102RR 11/91

INTERPOLL LABORATORIES, INC.
METER CALIBRATION SHEET
EPA METHOD 6

Control Module No. 10
Serial No. OTM 1334112
Wat Test Meter No. AL-20
Technician Ed T. [Signature]

[illegible]

Positive leak check performed by
 Water was in tolerance ☒
 Water was not in tolerance ☐; readjusted linkage
 Water was not in tolerance ☐; changed dry test meters

Approved by  Date 6/6/94

* Based on AL-20 wet test meter calibration in Nov. 1991 against Bell Prover (NBS Traceable) - Carl Poe Co.

50102RA 11/91

Date 4-13-57
Bar. Press. 28.66 in. Hg

**INTERPOLL LABORATORIES, INC.
METER CALIBRATION SHEET
EPA METHOD 5**

Control Module No. 14
Serial No. DTM 1334119
Net Test Meter No. AL-20
Technician E. J. Haskins

[illegible]

Positive leak check performed by
Water was in tolerance ☒

Water was not in tolerance ☐; readjusted linkage

Meter was not in tolerance ☒; changed dry test meters

Approved by Danish Khan Date 5/2/94

INTERPOLL LABORATORIES
MINIMODULE CALIBRATION SHEET
Flow Rate Range 0-0.13 CFM
(0-4 LPM)

Water Box No. 25

Serial No. DTW 69185

Wet Test Water No. AL-17 (.05 CF/REV)

Technician. S. BARNVILLE

Bar. Press. 29.14 in. Hg

[illegible]

Gas Meter Bimetallic Therm. Calibration/Verification

☐ $> +50\text{F}$ (Out of control) ☐ Recalibrated ☒

☒ $\leq 50F$ (In control) ☒ No action required

Water was in tolerance ☒; readjusted linkage ☐; changed dry test mo

Approved by Samir K. Dasgupta Date 11/14/94

* Verified against mercury in glass thermometer or calibrated platinum resistance thermometer.

**** Based on AL-17 wet test meter calibration in August 1989 against Bell Prover (NBS Traceable) - Carl Poe Co.**

50102R 8/89

1-13-94

1a. Hg

INTERPOL LABORATORIES

55

64711

NO. AL-17 (.05 CF/REV)

S. BANVILLE

10/11
Average:

~~SECRET~~

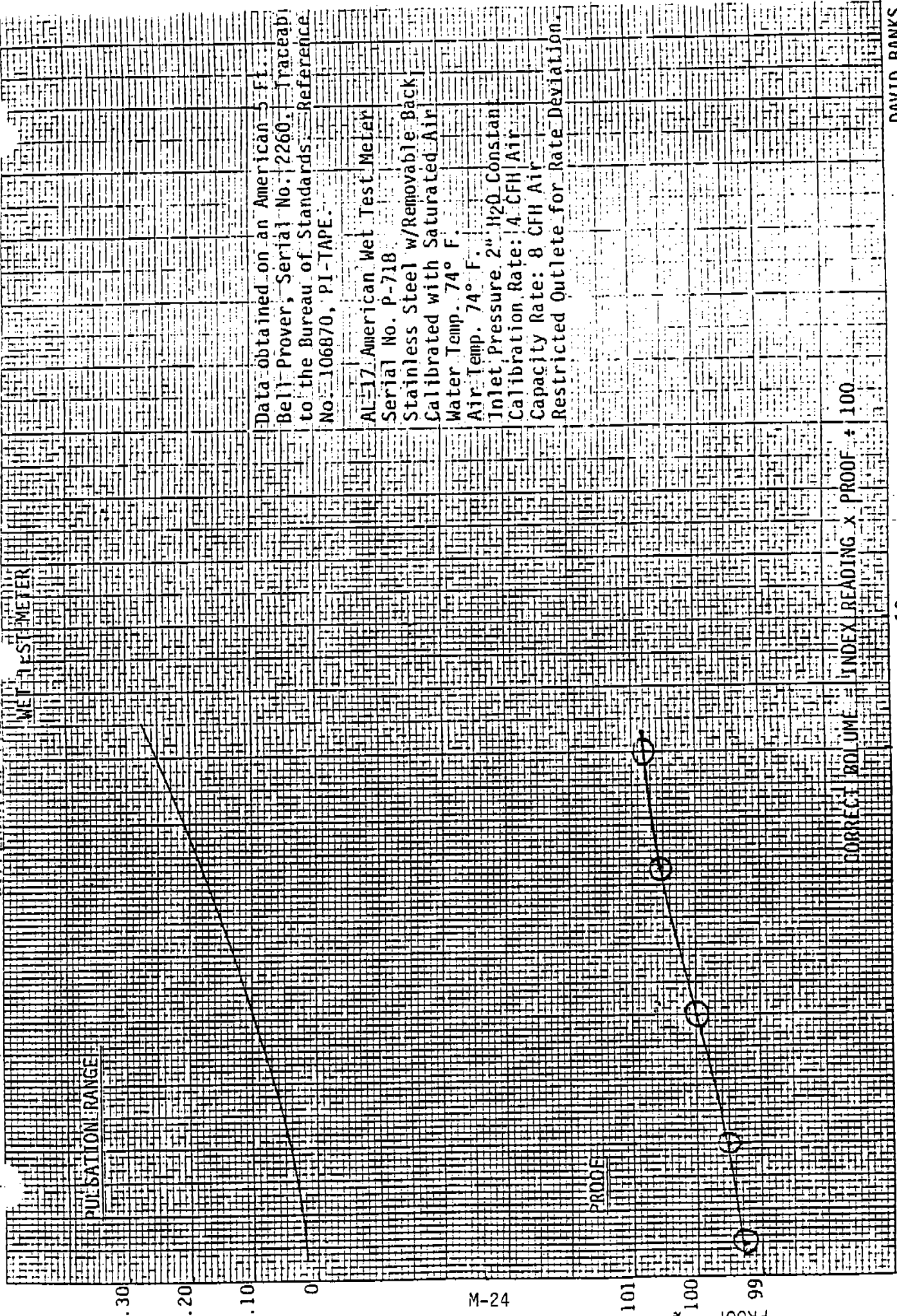
Calibrated

☒ No action required

Date 11/24/99

... (NBS Traceable) - Carl Poe Co.

DIFFERENTIAL PRESSURE METER TEST METER ROOF CALIBRATION CURVE



PROOF

PROOF

INDEX READING x PROOF = 100

DAVID BANKS
AUGUST, 1989

FLOW RATE - CUBIC FEET OF AIR PER HOUR

DIFFERENTIAL INCHES H2O

11-11-51

FLOW RATE CUBIC FEET OF AIR PER HOUR

ember, 1991

PULSATION RANGE

30

20

10

0

101

100

99

20

40

60

80

100

120

CORRECT VOLUME INDEX READING X PROOF = 100

DAVID BANKS

DIFFERENTIAL PRESSURE AND PROOF CALIBRATION CURVES

WET TEST METER

Calibrated with a 10 ft. American Bell
Prover, Serial No. 3157. Traceable to
the Bureau of Standards. Reference No.
5249068, PI-TAPE.

AL-20 American Met Test Meter

Serial No. 2117

Stainless Steel w/Removable Back

Calibrated w/Saturated Air

Water Temp. 74° F.

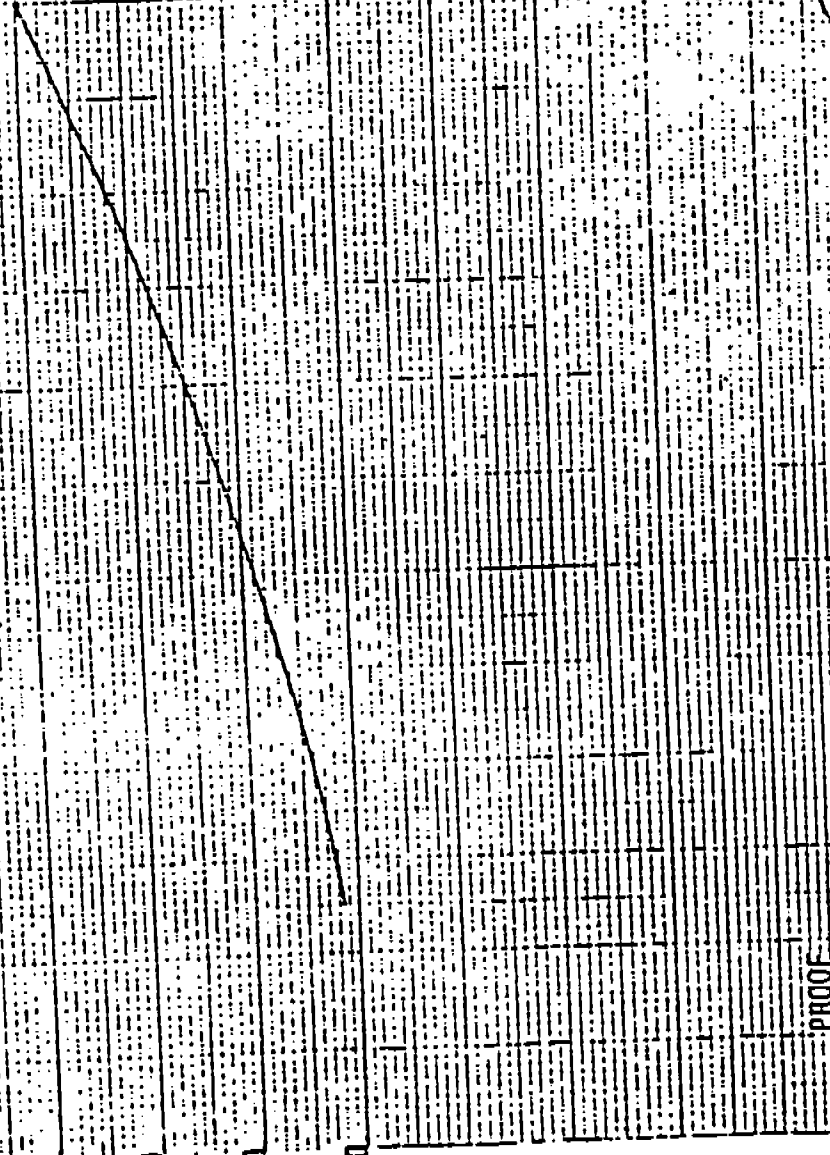
Air Temp. 74° F.

Inlet Pressure 2" H2O Constant

Calibration Rate: 60 CFH Per/Hr.

Capacity Rate: 120 CFH Per/Hr.

Restricted Outlet for Rate Deviation



Interpoll Laboratories, Inc.

(612) 786-6020

Nozzle Calibration

Data Sheet

Date of Calibration: 06-07-94

Nozzle Number 4-4

Technician: Scott Bainville

The nozzle is rotated in 60 degree increments and the diameter at each point is measured to the nearest 0.001 inch. The observed readings and average are shown below.

Position	Diameter (inches)
1	.251
2	.251
3	.251
Average:	.251

Interpoll Laboratories, Inc.
(612) 786-6020

Nozzle Calibration
Data Sheet

Date of Calibration: 06-07-94

Nozzle Number Glass

Technician: Scott Bainville

The nozzle is rotated in 60 degree increments and the diameter at each point is measured to the nearest 0.001 inch. The observed readings and average are shown below.

Position	Diameter (inches)
1	.270
2	.269
3	.270
Average:	.270

Interpoll Laboratories, Inc.
(612) 786-6020

Nozzle Calibration
Data Sheet

Date of Calibration: 06-07-94
Technician: Mark Kaehler

Nozzle Number MM5-6

The nozzle is rotated in 60 degree increments and the diameter at each point is measured to the nearest 0.001 inch. The observed readings and average are shown below.

Position	Diameter (inches)
1	.365
2	.363
3	.363
Average:	.364

Interpoll Laboratories, Inc.
(612) 786-6020

Nozzle Calibration
Data Sheet

Date of Calibration: 06-08-94

Nozzle Number 1-6

Technician: Ed Trowbridge

The nozzle is rotated in 60 degree increments and the diameter at each point is measured to the nearest 0.001 inch. The observed readings and average are shown below.

Position	Diameter (inches)
1	.354
2	.356
3	.355
Average:	.355

Interpoll Laboratories, Inc.
(612) 786-6020

**Nozzle Calibration
Data Sheet**

Date of Calibration: 06-08-94
Technician: Mark Kaehler

Nozzle Number 8-6

The nozzle is rotated in 60 degree increments and the diameter at each point is measured to the nearest 0.001 inch. The observed readings and average are shown below.

Position	Diameter (inches)
1	.364
2	.363
3	.363
Average:	.363

Interpoll Laboratories, Inc.

(612) 786-6020

Nozzle Calibration

Data Sheet

Date of Calibration: 06-08-94

Nozzle Number G-4

Technician: Scott Bainville

The nozzle is rotated in 60 degree increments and the diameter at each point is measured to the nearest 0.001 inch. The observed readings and average are shown below.

Position	Diameter (inches)
1	.225
2	.225
3	.225
Average:	.225

Interpoll Laboratories, Inc.
(612) 786-6020

Nozzle Calibration
Data Sheet

Date of Calibration: 06-08-94

Nozzle Number Glass

Technician: Duane Van Hoever

The nozzle is rotated in 60 degree increments and the diameter at each point is measured to the nearest 0.001 inch. The observed readings and average are shown below.

Position	Diameter (inches)
1	.245
2	.246
3	.247
Average:	.246

Interpoll Laboratories, Inc.
(612) 786-6020

Nozzle Calibration
Data Sheet

Date of Calibration: 06-08-94

Nozzle Number

Glass-6

Technician: Mark Kaehler

The nozzle is rotated in 60 degree increments and the diameter at each point is measured to the nearest 0.001 inch. The observed readings and average are shown below.

Position	Diameter (inches)
1	.369
2	.368
3	.367
Average:	.368

Interpoll Laboratories, Inc.
(612) 786-6020

Nozzle Calibration
Data Sheet

Date of Calibration: 06-09-94

Nozzle Number 4-3

Technician: Scott Bainville

The nozzle is rotated in 60 degree increments and the diameter at each point is measured to the nearest 0.001 inch. The observed readings and average are shown below.

Position	Diameter (inches)
1	.177
2	.177
3	.177
Average:	.177

Interpoll Laboratories, Inc.
(612) 786-6020

Nozzle Calibration
Data Sheet

Date of Calibration: 06-09-94

Nozzle Number Glass

Technician:

Duane Van Hoever

The nozzle is rotated in 60 degree increments and the diameter at each point is measured to the nearest 0.001 inch. The observed readings and average are shown below.

Position	Diameter (inches)
1	.189
2	.189
3	.188
Average:	.189

Interpoll Laboratories, Inc.
(612) 786-6020

Nozzle Calibration
Data Sheet

Date of Calibration: 06-09-94
Technician: Ed Trowbridge

Nozzle Number Glass

The nozzle is rotated in 60 degree increments and the diameter at each point is measured to the nearest 0.001 inch. The observed readings and average are shown below.

Position	Diameter (inches)
1	.446
2	.446
3	.445
Average:	.446

Interpoll Laboratories, Inc.
(612) 786-6020

Nozzle Calibration
Data Sheet

Date of Calibration: 06-09-94
Technician: Mark Kaehler

Nozzle Number MM5-7

The nozzle is rotated in 60 degree increments and the diameter at each point is measured to the nearest 0.001 inch. The observed readings and average are shown below.

Position	Diameter (inches)
1	.422
2	.423
3	.421
Average:	.422

Interpoll Laboratories, Inc.
(612) 786-6020

Nozzle Calibration
Data Sheet

Date of Calibration: 06-10-94

Nozzle Number 24-3

Technician: Mark Kaehler

The nozzle is rotated in 60 degree increments and the diameter at each point is measured to the nearest 0.001 inch. The observed readings and average are shown below.

Position	Diameter (inches)
1	.189
2	.188
3	.187
Average:	.188

Interpoll Laboratories, Inc.

(612) 786-6020

Nozzle Calibration

Data Sheet

Date of Calibration: 06-10-94

Nozzle Number Glass

Technician:

Duane Van Hoever

The nozzle is rotated in 60 degree increments and the diameter at each point is measured to the nearest 0.001 inch. The observed readings and average are shown below.

Position	Diameter (inches)
1	.240
2	.240
3	.240
Average:	.240

Interpoll Laboratories, Inc.

Temperature Measurement Device
Calibration Sheet

Unit under test:

Vendor OMEGA PDT-29
Model HH21 Serial Number T-97106
Range 0 - 2100 °F Thermocouple Type K
Date of Calibration 10-14-93 Technician SLB

Method of Calibration:

- ☐ Comparison against ASTM mercury in glass thermometer using a thermostatted and insulated aluminum block designed to provide uniform temperature. The temperature is adjusted by adjusting the voltage on the block heater cartridge.
- ☒ Omega Model CL-300 Type K Thermocouple Simulator which provides 22 precise temperature equivalent millivolt signals. The CL-300 is cold junction compensated. Calibration accuracy is $\pm 0.1\%$ of span (2100 °F) ± 1 degree (for negative temperatures add ± 2 degrees. The CL-300 simulates exactly the millivoltage of a Type K thermocouple at the indicated temperature.

Desired Temp (°F) Nominal	Temperature of Standard or Simulated Temp (°F)	Response of Unit Under Test (°F)	Deviation	
			Δt (°F)	(%)
0	0	-0.7	0.7	0.00
100	100	98.6	1.4	0.25
200	200	200.1	0.6	0.03
300	300	299.0	1.2	0.16
400	400	398.1	1.9	0.19
500	500	498.8	1.2	0.13
600	600	600.7	0.7	0.07
700	700	698.9	1.1	0.09
800	800	800.9	0.9	0.07
900	900	898.9	1.1	0.08
1000	1000	999.8	0.1	0.01
1100	1100	1098.5	1.4	0.09
1200	1200	1201.0	1.0	0.06
1300	1300	1295.7	1.3	0.07
1400	1400	1401.1	1.1	0.05
1500	1500	1499.4	1.6	0.08
1600	1600	1599.8	0.2	0.01
1700	1700	1697.9	2.2	0.10
1800	1800	1799.7	0.3	0.01
1900	1900	1897.0	3.0	0.13
2000	2000	1998.6	1.4	0.06
2100	2100	2097.0	3.0	0.12
		Averages:	1.22	0.09

OF = off scale response by unit under test (°F)
% dev = $100 \Delta t / (460 + t)$

- ☐ Unit in tolerance
☐ Unit was not in tolerance: recalibrated - See new calibration sheet.

Interpoll Laboratories, Inc.
Temperature Measurement Device
Calibration Sheet

Unit under test:

Vendor Omega Serial Number 735X1495
 Model H14 81 Thermocouple Type K
 Range 0 - 2100 °F Technician Mark Baehler
 Date of Calibration 4-8-77

Method of Calibration:



Comparison against ASTM mercury in glass thermometer using a thermostatted and insulated aluminum block to provide uniform temperature. The temperature is adjusted by adjusting the voltage on the block cartridge.



Omega Model CL-300 Type K Thermocouple Simulator which provides 22 precise temperature equivalent mV signals. The CL-300 is cold junction compensated. Calibration accuracy is $\pm 0.1\%$ of span (2100°F) ± 1 (for negative temperatures add ± 2 degrees. The CL-300 simulates exactly the millivoltage of a thermocouple at the indicated temperature.

Desired Temp (°F) Nominal	Temperature of Standard or Simulated Temp (°F)	Response of Unit Under Test (°F)	Deviation	
			Δt (°F)	(%)
0	0	-1	1	.2
100	100	100	0	0
200	200	201	1	.1
300	300	300	0	0
400	400	399	1	.1
500	500	499	1	.1
600	600	601	1	.1
700	700	700	0	0
800	800	802	2	.1
900	900	901	1	.1
1000	1000	1001	1	.1
1100	1100	1100	0	0
1200	1200	1202	2	.1
1300	1300	1300	0	0
1400	1400	1402	2	.1
1500	1500	1500	0	0
1600	1600	1603	3	.1
1700	1700	1701	1	.1
1800	1800	1803	3	.1
1900	1900	1901	1	.1
2000	2000	2001	1	.1
2100	2100	2099	1	.1
		Averages:	1.05	

OF = off scale response by unit under test (°F)
 $\% \text{ dev} = 100 \Delta t / (450 + t)$



Unit in tolerance

Unit was not in tolerance: recalibrated - See new calibration sheet.

Interpoll Laboratories, Inc.

Temperature Measurement Device
Calibration Sheet

Unit under test:

Vendor OMEGA
 Model HH 81
 Range -160 - 1372 C °F
 Date of Calibration 4-18-94
 Serial Number 74JX0223 #33
 Thermocouple Type K
 Technician BOB

Method of Calibration:

- ☐ Comparison against ASTM mercury in glass thermometer using a thermostatted and insulated aluminum block designed to provide uniform temperature. The temperature is adjusted by adjusting the voltage on the block heater cartridge.
- ☒ Omega Model CL-300 Type K Thermocouple Simulator which provides 22 precise temperature equivalent millivolt signals. The CL-300 is cold junction compensated. Calibration accuracy is $\pm 0.1\%$ of span (2100 °F) ± 1 degree (for negative temperatures add ± 2 degrees. The CL-300 simulates exactly the millivoltage of a Type K thermocouple at the indicated temperature.

Desired Temp (°F) Nominal	Temperature of Standard or Simulated Temp (°F)	Response of Unit Under Test (°F)	Deviation	
			Δt (°F)	(%)
0	0	-1.0	-1.0	-.21
100	100	98.5	1.5	.26
200	200	200.3	.3	.04
300	300	298.6	1.4	.18
400	400	398	2	.23
500	500	499	1	.10
600	600	600	0	0
700	700	699	1	.08
800	800	801	1	.07
900	900	900	0	0
1000	1000	1001	1	.06
1100	1100	1099	1	.06
1200	1200	1201	1	.06
1300	1300	1299	1	.05
1400	1400	1402	2	.01
1500	1500	1500	0	0
1600	1600	1603	3	.14
1700	1700	1701	1	.04
1800	1800	1803	3	.13
1900	1900	1901	1	.04
2000	2000	2001	1	.04
2100	2100	2099	1	.03
		Averages:	1.05	.064

OF = off scale response by unit under test (°F)
 $\% \text{ dev} = 100 \Delta t / (460 + t)$

☒ Unit in tolerance
☐ Unit was not in tolerance: recalibrated - See new calibration sheet.

Interpoll Laboratories, Inc.

Temperature Measurement Device
Calibration Sheet

E.T.'s

Unit under test:

Vendor

Omega

Model

HH 81

Range

0-2000

°F

Date of Calibration

4-21-74

Serial Number

74TX0343

Thermocouple Type

K

Technician

E. TROUBLED

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Method of Calibration:

- ☐ Comparison against ASTM mercury in glass thermometer using a thermostatted and insulated aluminum block to provide uniform temperature. The temperature is adjusted by adjusting the voltage on the block cartridge.
- ☒ Omega Model CL-300 Type K Thermocouple Simulator which provides 22 precise temperature equivalent signals. The CL-300 is cold junction compensated. Calibration accuracy is $\pm 0.1\%$ of span (2100 °F) $\pm$ (for negative temperatures add ± 2 degrees. The CL-300 simulates exactly the millivoltage of a thermocouple at the indicated temperature.

Desired Temp (°F) Nominal	Temperature of Standard or Simulated Temp (°F)	Response of Unit Under Test (°F)	Deviation	
			Δt (°F)	(%)
0	0	-1.9	-1.9	1.4
100	100	-97.5	-2.5	1.6
200	200	199.7	-1.3	1.6
300	300	297.5	-2.5	1.6
400	400	397	-3	1.6
500	500	498	-2	1.6
600	600	600		1.6
700	700	699	-1	1.6
800	800	801	+1	1.6
900	900	900		1.6
1000	1000	1001	+1	1.6
1100	1100	1098	-2	1.6
1200	1200	1201	+1	1.6
1300	1300	1299	-1	1.6
1400	1400	1402	+2	1.6
1500	1500	1500		1.6
1600	1600	1603	+3	1.6
1700	1700	1701	+1	1.6
1800	1800	1804	+4	1.6
1900	1900	1901	+1	1.6
2000	2000	2001	+1	1.6
2100	2100	2099	-1	1.6
		Averages:	1.46	1.1

OF = off scale response by unit under test (°F)
% dev = $100 \Delta t / (460 + t)$



Interpoll Laboratories, Inc.

Temperature Measurement Device Calibration Sheet

Unit under test:

Vendor

Omega

Model

HH-51

Range

0 - 2000

°F

Date of Calibration

7-21-94

Serial Number

74TX0332

Thermocouple Type

K

Technician

E. TROUBLED

Method of Calibration:



Comparison against ASTM mercury in glass thermometer using a thermostatted and insulated aluminum block designed to provide uniform temperature. The temperature is adjusted by adjusting the voltage on the block heater cartridge.



Omega Model CL-300 Type K Thermocouple Simulator which provides 22 precise temperature equivalent millivolt signals. The CL-300 is cold junction compensated. Calibration accuracy is $\pm 0.1\%$ of span (2100 °F) ± 1 degree (for negative temperatures add ± 2 degrees. The CL-300 simulates exactly the millivoltage of a Type K thermocouple at the indicated temperature.

Desired Temp (°F) Nominal	Temperature of Standard or Simulated Temp (°F)	Response of Unit Under Test (°F)	Deviation	
			Δt (°F)	(%)
0	0	-3	-3	.65
100	100	98	-2	.35
200	200	200	0	0
300	300	298	-2	.30
400	400	398	-2	.23
500	500	499	-1	.10
600	600	601	+1	.09
700	700	699	-1	.09
800	800	801	+1	.08
900	900	900	0	0
1000	1000	1001	+1	.07
1100	1100	1100	0	0
1200	1200	1201	+1	.06
1300	1300	1299	-1	.05
1400	1400	1402	+2	.11
1500	1500	1501	+1	.05
1600	1600	1604	+4	.19
1700	1700	1701	+1	.05
1800	1800	1804	+4	.18
1900	1900	1901	+1	.04
2000	2000	2001	+1	.04
2100	2100	2099	-1	.04
		Averages:	1.40	.123

OF = off scale response by unit under test (°F)

% dev = $100 \Delta t / (460 + t)$



Unit in tolerance



Unit was not in tolerance: recalibrated - See new calibration sheet.

S-Type Pitot Tube Inspection Sheet

Pitot Tube No. 22-5

Pitot tube dimensions:

1. External tubing diameter (D_t) .316 IN.
2. Base to Side A opening plane (P_A) .460 IN.
3. Base to Side B opening plane (P_B) .460 IN.

Alignment:

4. α_1 $< 10^\circ$ 0
5. α_2 $< 10^\circ$ 0
6. B_1 $< 5^\circ$ 0
7. B_2 $< 5^\circ$ 0
8. Z $< .125"$.02
9. W $< .0625"$.02

Distance from Pitot to Probe Components:

10. Pitot to 0.500 IN. nozzle .750 IN.
11. Pitot to probe sheath 3.0 IN.
12. Pitot to thermocouple (parallel to probe) 3.0 IN.
13. Pitot to thermocouple (perpendicular to probe) 760 IN.

- ☒ Meets all EPA design criteria thus $C_p = 0.84$
☐ Does not meet EPA design criteria - thus calibrate in wind tunnel.
 $C_p =$ _____

Date of Inspection:

4-8-84

Inspected by:

[Signature]

S-Type Pitot Tube Inspection Sheet

Pitot Tube No. 22-6

Pitot tube dimensions:

1. External tubing diameter (D) 316 IN.
2. Base to Side A opening plane (P_A) 460 IN.
3. Base to Side B opening plane (P_B) 460 IN.

Alignment:

4. α_1 < 10° 0
5. α_2 < 10° 0
6. B_1 < 5° 0
7. B_2 < 5° 0
8. Z < .125" .02
9. W < .0625" .02

Distance from Pitot to Probe Components:

10. Pitot to 0.500 IN. nozzle 750 IN.
11. Pitot to probe sheath 3.0 IN.
12. Pitot to thermocouple (parallel to probe) 3.0 IN.
13. Pitot to thermocouple (perpendicular to probe) 760 IN.

- ☒ Meets all EPA design criteria thus $C_p = 0.84$
☐ Does not meet EPA design criteria - thus calibrate in wind tunnel.
 $C_p =$ _____

Date of Inspection:

4-8-84

Inspected by:

[Signature]

S-Type Pitot Tube Inspection Sheet

Pitot Tube No. 22-8

Pitot tube dimensions:

1. External tubing diameter (D_e) .316 IN.
2. Base to Side A opening plane (P_A) .460 IN.
3. Base to Side B opening plane (P_B) .460 IN.

Alignment:

4. α_1 $< 10^\circ$ 0
5. α_2 $< 10^\circ$ 0
6. B_1 $< 5^\circ$ 0
7. B_2 $< 5^\circ$ 0
8. Z $< .125"$.0
9. W $< .0625"$.01

Distance from Pitot to Probe Components:

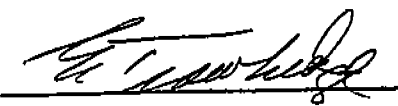
10. Pitot to 0.500 IN. nozzle .760 IN.
11. Pitot to probe sheath 3.0 IN.
12. Pitot to thermocouple (parallel to probe) 3.0 IN.
13. Pitot to thermocouple (perpendicular to probe) .760 IN.

- ☒ Meets all EPA design criteria thus $C_p = 0.84$
☐ Does not meet EPA design criteria - thus calibrate in wind tunnel.
 $C_p =$ _____

Date of Inspection:

1-8-94

Inspected by:



S-Type Pitot Tube Inspection Sheet

Pitot Tube No 24-5

Pitot tube dimensions:

1. External tubing diameter (D) .316 IN.
2. Base to Side A opening plane (P_A) .460 IN.
3. Base to Side B opening plane (P_B) .460 IN.

Alignment:

4. α_1 < 10° 0
5. α_2 < 10° 0

6. β_1 < 5° 0
7. β_2 < 5° 0

8. Z < .125" .02
9. W < .0625" 0

Distance from Pitot to Probe Components:

10. Pitot to 0.500 IN. nozzle .760 IN.
11. Pitot to probe sheath 3.0 IN.
12. Pitot to thermocouple (parallel to probe) 3.0 IN.
13. Pitot to thermocouple (perpendicular to probe) .750 IN.

- ☒ Meets all EPA design criteria thus $C_p = 0.84$
☐ Does not meet EPA design criteria - thus calibrate in wind tunnel.
 $C_p =$ _____

Date of Inspection:

4-8-94

Inspected by:

[Signature]

S-Type Pitot Tube Inspection Sheet

Pitot Tube No. 24-8

Pitot tube dimensions:

1. External tubing diameter (D) .316 IN.
2. Base to Side A opening plane (P_A) .460 IN.
3. Base to Side B opening plane (P_B) .460 IN.

Alignment:

4. α_1 < 10° 0
5. α_2 < 10° 0
6. β_1 < 5° 0
7. β_2 < 5° 0
8. Z < .125" 0
9. W < .0625" .025

Distance from Pitot to Probe Components:

10. Pitot to 0.500 IN. nozzle .760 IN.
11. Pitot to probe sheath 3.0 IN.
12. Pitot to thermocouple (parallel to probe) 3.0 IN.
13. Pitot to thermocouple (perpendicular to probe) .752 IN.

- ☒ Meets all EPA design criteria thus $C_p = 0.84$
☐ Does not meet EPA design criteria - thus calibrate in wind tunnel.
 $C_p =$ _____

Date of Inspection:

4-8-84

Inspected by:

[Signature]

S-Type Pitot Tube Inspection Sheet

Pitot Tube No. 29-6

Pitot tube dimensions:

1. External tubing diameter (D_t) .316 IN.
2. Base to Side A opening plane (P_A) .460 IN.
3. Base to Side B opening plane (P_B) .460 IN.

Alignment:

4. α_1 $< 10^\circ$ 0
5. α_2 $< 10^\circ$ 0

6. B_1 $< 5^\circ$ 0
7. B_2 $< 5^\circ$ 0

8. Z $< .125"$.02
9. W $< .0625"$.02

Distance from Pitot to Probe Components:

10. Pitot to 0.500 IN. nozzle .750 IN.
11. Pitot to probe sheath 3.0 IN.
12. Pitot to thermocouple (parallel to probe) 3.0 IN.
13. Pitot to thermocouple (perpendicular to probe) .760 IN.

- ☒ Meets all EPA design criteria thus $C_p = 0.84$
☐ Does not meet EPA design criteria - thus calibrate in wind tunnel.
 $C_p =$ _____

Date of Inspection:

4-7-94

Inspected by:

[Signature]

S-Type Pitot Tube Inspection Sheet

Pitot Tube No. MM-6

Pitot tube dimensions:

1. External tubing diameter (D) .316 IN.
2. Base to Side A opening plane (P_A) .460 IN.
3. Base to Side B opening plane (P_B) .460 IN.

Alignment:

4. α_1 < 10° 0
5. α_2 < 10° 0
6. B_1 < 5° 0
7. B_2 < 5° 0
8. Z < .125" .03
9. W < .0625" .025

Distance from Pitot to Probe Components:

10. Pitot to 0.500 IN. nozzle .750 IN.
11. Pitot to probe sheath 3.0 IN.
12. Pitot to thermocouple (parallel to probe) 3.0 IN.
13. Pitot to thermocouple (perpendicular to probe) .760 IN.

- ☒ Meets all EPA design criteria thus $C_p = 0.84$
☐ Does not meet EPA design criteria - thus calibrate in wind tunnel.
 $C_p =$ _____

Date of Inspection:

4-8-94

Inspected by:

[Signature]

Interpoll Laboratories, Inc.
(612) 786-6020

S-Type Pitot Tube Inspection Sheet

Pitot Tube No. MM5-8

Pitot tube dimensions:

1. External tubing diameter (D_t) .316 IN.
2. Base to Side A opening plane (P_A) .460 IN.
3. Base to Side B opening plane (P_B) .460 IN.

Alignment:

4. α_1 $< 10^\circ$ 0
5. α_2 $< 10^\circ$ 0

6. B_1 $< 5^\circ$ 2
7. B_2 $< 5^\circ$ 2

8. Z $< .125"$.02
9. W $< .0625"$.02

Distance from Pitot to Probe Components:

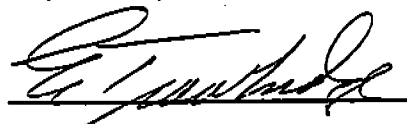
10. Pitot to 0.500 IN. nozzle .750 IN.
11. Pitot to probe sheath 3.0 IN.
12. Pitot to thermocouple (parallel to probe) 3.0 IN.
13. Pitot to thermocouple (perpendicular to probe) .760 IN.

- ☒ Meets all EPA design criteria thus $C_p = 0.84$
☐ Does not meet EPA design criteria - thus calibrate in wind tunnel.
 $C_p =$ _____

Date of Inspection:

4-7-93

Inspected by:



CFR Title 40 Part 60 Appenidix A Method 2

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4-7-93 CASTACKIWPFORMS-S-348

INTERPOLL LABORATORIES

(612)786-6020

Stack Sampling Department - QA
Aneroid Barometer Calibration Sheet

Date 2-18-74
Technician BoB
Mercury Column Barometer No. LAB 1
Aneroid Barometer No. 10723029

Actual Mercury Barometer Read	Ambient Temp.	Temperature Correction Factor	Adjusted Mercury Barometer Read	Initial Aneroid Barometer Read	Difference (Pba-Pbm)
29.01	76	.125	28.885	28.83	.055

Has this barometer shown any consistent problems with calibration? Yes/No.
yes, explain. NO

Has problem been alleviated? Yes/No. How? _____

***Note**

Aneroid barometers will be calibrated periodically against a mercury column barometer. The aneroid barometer to be calibrated should be placed in close proximity to the mercury barometer and left to equilibrate for 20-30 minutes before calibrating. Aneroid barometer will be calibrated to the adjusted mercury barometer readings.

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INTERPOLL LABORATORIES

(612)786-6020

Stack Sampling Department - QA
Aneroid Barometer Calibration Sheet

Date 10-15-93
Technician SCOTT L BAINVILLE
Mercury Column Barometer No. 1
Aneroid Barometer No. 560209

Actual Mercury Barometer Read	Ambient Temp.	Temperature Correction Factor	Adjusted Mercury Barometer Read	Initial Aneroid Barometer Read	Difference (Pba-Pbm)
29.10	76	.134	28.97	29.16	0.19
29.13	73	.124	29.01	29.19	0.18

Has this barometer shown any consistent problems with calibration? Yes/No. If yes, explain. NO

Has problem been alleviated? Yes/No. How? N/A

***Note**

Aneroid barometers will be calibrated periodically against a mercury column barometer. The aneroid barometer to be calibrated should be placed in close proximity to the mercury barometer and left to equilibrate for 20-30 minutes before calibrating. Aneroid barometer will be calibrated to the adjusted mercury barometer readings.

S-312

INTERPOLL LABORATORIES

(612)786-6020

Stack Sampling Department - QA
Aneroid Barometer Calibration Sheet

Date 9-13-93
Technician M. A. Goshen
Mercury Column Barometer No. LAB-1
Aneroid Barometer No. 560815

Actual Mercury Barometer Read	Ambient Temp.	Temperature Correction Factor	Adjusted Mercury Barometer Read	Initial Aneroid Barometer Read	Difference (P _{ba} -P _{bm})
28.770	72	.114	28.656	28.760	.104

Has this barometer shown any consistent problems with calibration? Yes (No) If yes, explain. _____

Has problem been alleviated? Yes/No. How? _____

***Note**

Aneroid barometers will be calibrated periodically against a mercury column barometer. The aneroid barometer to be calibrated should be placed in close proximity to the mercury barometer and left to equilibrate for 20-30 minutes before calibrating. Aneroid barometer will be calibrated to the adjusted mercury barometer readings.

S-312

INTERPOLL LABORATORIES

(612)786-6020

Stack Sampling Department - QA
Aneroid Barometer Calibration Sheet

ET'S

Date 5-31-94
Technician E. T. S.
Mercury Column Barometer No. LAB 1
Aneroid Barometer No. ultrameter model 12 SN-01002-084

Actual Mercury Barometer Read	Ambient Temp.	Temperature Correction Factor	Adjusted Mercury Barometer Read	Initial Aneroid Barometer Read	Difference (Pba-Pbm)
29.230	72	.115	29.115	29.12	.005

Has this barometer shown any consistent problems with calibration? Yes/No. If yes, explain. no

Has problem been alleviated? Yes/No. How? _____

*Note

Aneroid barometers will be calibrated periodically against a mercury column barometer. The aneroid barometer to be calibrated should be placed in close proximity to the mercury barometer and left to equilibrate for 20-30 minutes before calibrating. Aneroid barometer will be calibrated to the adjusted mercury barometer readings.

S-312

INTERPOLL LABORATORIES

(612)786-6020

Stack Sampling Department - QA
Aneroid Barometer Calibration Sheet

Date 2/16/94
Technician D. Van Hoever
Mercury Column Barometer No. 1
Aneroid Barometer No. _____

Actual Mercury Barometer Read	Ambient Temp.	Temperature Correction Factor	Adjusted Mercury Barometer Read	Initial Aneroid Barometer Read	Difference (P _{ba} -P _{bm})
29.23	76	.124	29.11	29.10	.01

Has this barometer shown any consistent problems with calibration? Yes/No. No. If yes, explain. _____

Has problem been alleviated? Yes/No. How? _____

*Note

Aneroid barometers will be calibrated periodically against a mercury column barometer. The aneroid barometer to be calibrated should be placed in close proximity to the mercury barometer and left to equilibrate for 20-30 minutes before calibrating. Aneroid barometer will be calibrated to the adjusted mercury barometer readings.

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