

Note: This is a reference cited in *AP 42, Compilation of Air Pollutant Emission Factors, Volume I Stationary Point and Area Sources*. AP42 is located on the EPA web site at www.epa.gov/ttn/chief/ap42/

The file name refers to the reference number, the AP42 chapter and section. The file name "ref02_c01s02.pdf" would mean the reference is from AP42 chapter 1 section 2. The reference may be from a previous version of the section and no longer cited. The primary source should always be checked.

**REPORT OF AIR
EMISSIONS AND INLET LOADING TESTS
FOR
LOUISIANA PACIFIC CORPORATION
URANIA MDF PLANT**

**Urania, Louisiana
January 18 through 21, 1994**

**Prepared for
Louisiana Pacific Corporation
Post Office Box 3107
Conroe, Texas 77305**

**ph: 409/760-5921
Contact: Dr. James T. Boswell**

**Performed By:
Environmental Monitoring Laboratories
Ridgeland, Mississippi
(601-856-3092)**

EMISSION TEST REPORT REVIEW SUMMARY**Source Category:**

Filename: mdf2.xls
Ref. No.: 2(OECA)
Date: 14-Jul-97
Reviewer: DRL

Facility: Louisiana Pacific Corporation
Location: Urania, Louisiana
Source: Press Vent RTO Stack
Test date: 20-Jan-94 21-Jan-94

Test ID	Parameter	Units	Values reported			
			Run 1	Run 2	Run 3	AVERAGE
Total Inlet Emissions						
	Filterable PM	lb/hr	1.68	1.57	1.35	1.54
	Condensable inorg. PM	lb/hr	0.36	0.69	0.86	0.64
	Condensable org. PM	lb/hr	0.48	0.65	0.62	0.58
	Total condensable PM	lb/hr	0.84	1.34	1.48	1.22
	TOC as CARBON	lb/hr	2.88	2.63	3.10	2.87
	Formaldehyde	lb/hr	11.72	10.10	8.24	10.02
Total Outlet Emissions						
rto	Filterable PM	lb/hr	0.35	0.43	0.30	0.36
	Condensable inorg. PM	lb/hr	0.04	0.03	0.11	0.06
	Condensable org. PM	lb/hr	0.01	0.13	0.10	0.08
	Total condensable PM	lb/hr	0.05	0.16	0.21	0.14
		TOC as CARBON	lb/hr	0.17	0.26	0.20
	Formaldehyde	lb/hr	0.11	0.08	0.06	0.08
Control Efficiency						
	Filterable PM	%	79.0	72.8	77.9	76.6
	Condensable inorg. PM	%	88.6	95.9	86.7	90.4
	Condensable org. PM	%	97.2	80.1	84.0	87.1
	Total condensable PM	%	93.5	88.2	85.6	89.1
	TOC	%	94.2	90.2	93.4	92.6
	Formaldehyde	%	99.0	99.2	99.3	99.2

EMISSION TEST REPORT REVIEW SUMMARY

Source Category:

Filename: mdf2.xls
 Ref. No.: 2(OECA)
 Date: 11-Jul-97
 Reviewer: DRL

Facility: Louisiana Pacific Corporation
 Location: Urania, Louisiana
 Source: Press Vent RTO Inlet
 Test date: 21-Jan-94

Emission Data/Mass Flux Rates/Emission Factors

Test ID	Parameter	Units	Values reported			
			Run 1	Run 2	Run 3	AVERAGE
	Stack temperature	Deg F	81.3	83.3	95.5	86.7
	Pressure	in. Hg	30.1	30.1	30.1	30.1
	Moisture	%	1.3	0.9	1.2	1.1
	Oxygen	%	20.9	20.9	20.9	20.9
	Gas volume sampled	dscf	40.81	40.95	40.49	40.75
	Vol. flow, actual	acfm	66,946	68,931	69,475	68,451
	Vol. flow, standard*	dscfm	64,894	66,802	65,691	65,796
	Isokinetic variation	%	95.3	92.9	93.4	93.9
	Process rate	MSF 3/4/hr	9.0	9.0	9.0	9.0
Indicate basis for process rate:			thouthand square feet of 3/4 thick board per hour			
Pollutant mass:						
	Filterable PM	grams	0.008	0.0073	0.0063	7.20E-03
	Condensable inorg. PM	grams	0.0017	0.0032	0.004	2.97E-03
	Condensable org. PM	grams	0.0023	0.003	0.0029	2.73E-03
	Total condensable PM	grams	0.004	0.0062	0.0069	5.70E-03
Pollutant concentrations:						
	Filterable PM	gr/dscf	3.02E-03	2.75E-03	2.40E-03	2.73E-03
	Condensable inorg. PM	gr/dscf	6.43E-04	1.21E-03	1.52E-03	1.12E-03
	Condensable org. PM	gr/dscf	8.70E-04	1.13E-03	1.11E-03	1.04E-03
	Total condensable PM	gr/dscf	1.51E-03	2.34E-03	2.63E-03	2.16E-03
	CO2	% vol.	0.0	0.0	0.0	0.00E+00
	NOx	ppmdv	0.0	0.0	0.0	0.00E+00
	CO	ppmdv	0.0	0.0	0.0	0.00E+00
Pollutant mass flux rates:						
	Filterable PM	lb/hr	1.68E+00	1.57E+00	1.35E+00	1.54E+00
	Condensable inorg. PM	lb/hr	3.58E-01	6.90E-01	8.58E-01	6.35E-01
	Condensable org. PM	lb/hr	4.84E-01	6.47E-01	6.22E-01	5.84E-01
	Total condensable PM	lb/hr	8.41E-01	1.34E+00	1.48E+00	1.22E+00
	CO2	lb/hr	0.00E+00	0.00E+00	0.00E+00	0.00E+00
	NOx	lb/hr	0.00E+00	0.00E+00	0.00E+00	0.00E+00
	CO	lb/hr	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Emission factors (ENGLISH UNITS):						
	Filterable PM	lb/unit	1.88E-01	1.76E-01	1.51E-01	1.71E-01
	Condensable inorg. PM	lb/unit	3.99E-02	7.71E-02	9.58E-02	7.09E-02
	Condensable org. PM	lb/unit	5.40E-02	7.22E-02	6.94E-02	6.52E-02
	Total condensable PM	lb/unit	9.39E-02	1.49E-01	1.65E-01	1.36E-01
	CO2	lb/unit	0.00E+00	0.00E+00	0.00E+00	0.00E+00
	NOx	lb/unit	0.00E+00	0.00E+00	0.00E+00	0.00E+00
	CO	lb/unit	0.00E+00	0.00E+00	0.00E+00	0.00E+00

*DSCFM BASED ON A STANDARD TEMPERATURE OF 68 DEGREES FAHRENHEIT

EMISSION TEST REPORT REVIEW SUMMARY

Source Category:

Filename: mdf2.xls
 Ref. No.: 2(OECA)
 Date: 11-Jul-97
 Reviewer: DRL

Facility: Louisiana Pacific Corporation
 Location: Urania, Louisiana
 Source: Press Vent RTO Inlet
 Test date: 20-Jan-94

Emission Data/Mass Flux Rates/Emission Factors

Test ID	Parameter	Units	Values reported			
			Run 1	Run 2	Run 3	AVERAGE
	Stack temperature	Deg F	101.6	97.6	97.9	99.0
	Pressure	in. Hg	30.1	30.1	30.1	30.1
	Moisture	%	0.8	1.1	1.0	0.9
	Oxygen	%	20.9	20.9	20.9	20.9
	Gas volume sampled	dscf	61.80	72.10	60.95	64.95
	Vol. flow, actual	acfm	70,878	80,996	69,798	73,891
	Vol. flow, standard*	decfm	66,509	76,332	65,817	69,553
	Isokinetic variation	%	99.1	100.7	98.7	99.5
	Process rate	MSF 3/4/hr	9.1	9.1	9.1	9.1
Indicate basis for process rate:			thouthand square feet of 3/4 thick board per hour			
	Pollutant concentrations:		AVERAGE			
	TOC as propane	ppmwv	6.28E+00	4.97E+00	6.80E+00	
	TOC as propane	ppmdv	6.3	5.0	6.9	6.07E+00
	CO2	% vol.	0.0	0.0	0.0	0.00E+00
	Formaldehyde	ppmdv	37.725	28.333	26.793	3.10E+01
	Pollutant mass flux rates:		AVERAGE			
	TOC as propane	lb/hr	2.88E+00	2.63E+00	3.10E+00	2.87E+00
	CO2	lb/hr	0.00E+00	0.00E+00	0.00E+00	0.00E+00
	Formaldehyde	lb/hr	1.17E+01	1.01E+01	8.24E+00	1.00E+01
	Emission factors (ENGLISH UNITS):		AVERAGE			
	TOC as propane	lb/unit	3.18E-01	2.89E-01	3.41E-01	3.16E-01
	CO2	lb/unit	0.00E+00	0.00E+00	0.00E+00	0.00E+00
	Formaldehyde	lb/unit	1.29E+00	1.11E+00	9.07E-01	1.10E+00

*DSCFM BASED ON A STANDARD TEMPERATURE OF 68 DEGREES FAHRENHEIT

TOC on Gasolene = 0.24 12/13/94

EMISSION TEST REPORT REVIEW SUMMARY

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Date: 11-Jul-97
Reviewer: DRL

Facility: Louisiana Pacific Corporation
Location: Urania, Louisiana
Source: Press Vent RTO Stack
Test date: 21-Jan-94

Emission Data/Mass Flux Rates/Emission Factors

Test ID	Parameter	Units	Values reported			
			Run 1	Run 2	Run 3	AVERAGE
rto	Stack temperature	Deg F	193.9	197.9	208	199.9
	Pressure	in. Hg	30.3	30.3	30.3	30.3
	Moisture	%	1.2	1.4	1.6	1.4
	Oxygen	%	20.9	20.9	20.9	20.9
	Gas volume sampled	dscf	69.20	68.19	68.20	68.53
	Vol. flow, actual	acfm	88,009	92,058	93,392	91,153
	Vol. flow, standard*	dscfm	71,025	73,699	73,465	72,730
	Isokinetic variation	%	98.5	93.5	93.8	95.3
	Process rate	MSF 3/4/hr	9.0	9.0	9.0	9.0
	Indicate basis for process rate: thouthand square feet of 3/4 thick board per hour					
	Pollutant mass:					
	Filterable PM	grams	0.0026	0.003	0.0021	2.57E-03
	Condensable inorg. PM	grams	0.0003	0.0002	0.0008	4.33E-04
	Condensable org. PM	grams	0.0001	0.0009	0.0007	5.67E-04
	Total condensable PM	grams	0.0004	0.0011	0.0015	1.00E-03
	Pollutant concentrations:					
	Filterable PM	gr/dscf	5.80E-04	6.79E-04	4.75E-04	5.78E-04
	Condensable inorg. PM	gr/dscf	6.69E-05	4.53E-05	1.81E-04	9.77E-05
	Condensable org. PM	gr/dscf	2.23E-05	2.04E-04	1.58E-04	1.28E-04
	Total condensable PM	gr/dscf	8.92E-05	2.49E-04	3.39E-04	2.26E-04
	CO2	% vol.	0.0	0.0	0.0	0.00E+00
	NOx	ppmdv	9.4	8.3	8.8	8.83E+00
	CO	ppmdv	3.1	2.0	2.1	2.40E+00
	Pollutant mass flux rates:					
	Filterable PM	lb/hr	3.53E-01	4.29E-01	2.99E-01	3.60E-01
	Condensable inorg. PM	lb/hr	4.07E-02	2.86E-02	1.14E-01	6.11E-02
	Condensable org. PM	lb/hr	1.36E-02	1.29E-01	9.97E-02	8.07E-02
	Total condensable PM	lb/hr	5.43E-02	1.57E-01	2.14E-01	1.42E-01
	CO2	lb/hr	0.00E+00	0.00E+00	0.00E+00	0.00E+00
	NOx	lb/hr	4.78E+00	4.38E+00	4.63E+00	4.60E+00
	CO	lb/hr	9.60E-01	6.43E-01	6.73E-01	7.58E-01
	Emission factors (ENGLISH UNITS):					
	Filterable PM	lb/unit	3.94E-02	4.79E-02	3.34E-02	4.02E-02
	Condensable inorg. PM	lb/unit	4.54E-03	3.19E-03	1.27E-02	6.82E-03
	Condensable org. PM	lb/unit	1.51E-03	1.44E-02	1.11E-02	9.00E-03
	Total condensable PM	lb/unit	6.06E-03	1.75E-02	2.39E-02	1.58E-02
	CO2	lb/unit	0.00E+00	0.00E+00	0.00E+00	0.00E+00
	NOx	lb/unit	5.34E-01	4.89E-01	5.17E-01	5.13E-01
	CO	lb/unit	1.07E-01	7.17E-02	7.51E-02	8.47E-02

*DSCFM BASED ON A STANDARD TEMPERATURE OF 68 DEGREES FAHRENHEIT

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Facility: Louisiana Pacific Corporation
 Location: Urania, Louisiana
 Source: Press Vent RTO Stack
 Test date: 20-Jan-94

Emission Data/Mass Flux Rates/Emission Factors

Test ID	Parameter	Units	Values reported			
			Run 1	Run 2	Run 3	AVERAGE
rto	Stack temperature	Deg F	211.4	216	210.9	212.8
	Pressure	in. Hg	30.3	30.3	30.3	30.3
	Moisture	%	1.7	1.9	1.6	1.7
	Oxygen	%	20.9	20.9	20.9	20.9
	Gas volume sampled	dscf	45.05	53.81	45.04	47.97
	Vol. flow, actual	acfm	92,812	110,916	93,747	99,158
	Vol. flow, standard*	dscfm	72,667	86,075	73,491	77,411
	Isokinetic variation	%	93.4	94.2	92.4	93.3
	Process rate	MSF 3/4/hr	9.1	9.1	9.1	9.1
Indicate basis for process rate:			thouthand square feet of 3/4 thick board per hour			
	Pollutant concentrations:					AVERAGE
	TOC as propane	ppmwv	3.30E-01	4.30E-01	4.00E-01	
	TOC as propane	ppmdv	0.3	0.4	0.4	3.94E-01
	CO2	% vol.	0.0	0.0	0.0	0.00E+00
	Formaldehyde	ppmdv	0.335	0.191	0.169	2.32E-01
	Pollutant mass flux rates:					AVERAGE
	TOC as propane	lb/hr	1.67E-01	2.58E-01	2.05E-01	2.10E-01
	CO2	lb/hr	0.00E+00	0.00E+00	0.00E+00	0.00E+00
	Formaldehyde	lb/hr	1.14E-01	7.68E-02	5.80E-02	8.29E-02
	Emission factors (ENGLISH UNITS):					AVERAGE
	TOC as propane	lb/unit	1.84E-02	2.85E-02	2.26E-02	2.31E-02
	CO2	lb/unit	0.00E+00	0.00E+00	0.00E+00	0.00E+00
	Formaldehyde	lb/unit	1.25E-02	8.46E-03	6.39E-03	9.12E-03

*DSCFM BASED ON A STANDARD TEMPERATURE OF 68 DEGREES FAHRENHEIT

NOC as propane = 0.019 MSF/hr

DENERS RTO Control Efficiency - PM

NORTH RTO	Filt PM, 16/hr	7.21
	Cond. PM, 16/hr	0.72

SOUTH RTO	Filt PM, 16/hr	8.29
	Cond. PM, 16/hr	

RTO INLET	Filt PM, 16/hr	83.6
	Cond. PM, 16/hr	3.9

Filt PM = 81 %

Cond. PM =

ENVIRONMENTAL MONITORING LABORATORIES, INC.

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February 17, 1994

Subject: Louisiana Pacific Corporation
Urania, Louisiana MDF Plant

During the period January 18 through 21, 1994, Environmental Monitoring Laboratories conducted air emissions and inlet loading tests at Louisiana Pacific Corporation's MDF facility in Urania, Louisiana. Testing was performed to determine emissions of particulate matter (PM), volatile organic compounds (VOC), formaldehyde (HCOH) nitrogen oxides (NOx), and carbon monoxide (CO) from the regenerative thermal oxidizer (RTO) system controlling emissions from two MDF dryers and from the RTO controlling emissions from the press vent. Testing was also simultaneously performed at the RTO inlets to determine removal efficiency.

Results:

DRYERS RTO	PM		VOC		HCOH		CO		NOx	
	gr/dscf	#/hr	ppm as C	#/hr	ppm	#/hr	ppm	#/hr	ppm	#/hr
NORTH RTO	0.012	7.93	5.36	0.22	1.19	0.41	3.4	1.10	27.3	14.6
SOUTH RTO	0.012	8.29	0.5	0.08	1.23	0.47	< 1	.11	27.2	15.2
RTO INLET	0.060	87.5	177	17.1	7.84	6.11	12.9	9.40	23.3	27.6
REMOVAL EFFICIENCY	81.46		98.25		85.60		88.30		-7.97	

PRESS VENT RTO	PM		VOC		HCOH		CO		NOx	
	gr/dscf	#/hr	ppm as C	#/hr	ppm	#/hr	ppm	#/hr	ppm	#/hr
OUTLET	0.0006	0.35	1.18	0.056	0.23	0.08	2.4	0.76	8.8	4.58
RTO INLET	0.0049	2.78	18.2	0.776	30.95	10.03	ND*	ND*	ND*	ND*
REMOVAL EFFICIENCY	87.41		92.78		99.20		N/A		N/A	

* ND means non-detected

The testing project was coordinated by Dr. James T. Boswell of Louisiana Pacific Corporation. Danny Russell of Environmental Monitoring Laboratories coordinated sample collection and analysis and report preparation. Armstrong Environmental performed testing at the dryers South RTO outlet. All formaldehyde samples were shipped to Air Techniques in Marietta, Georgia for analysis and reagent QA/QC. Mr. Paul Laird of the Louisiana Department of Environmental Quality was present to witness portions of the testing. Mr. David Chiles, Mr. Russell Karon, and Mr. Jerry May representing Smith Engineering Company were also present.

Following is a report of the testing.

REPORT OF AIR EMISSIONS AND INLET LOADING TESTS
FOR LOUISIANA PACIFIC CORPORATION
URANIA MDF PLANT
URANIA, LOUISIANA
JANUARY 18 THROUGH 21, 1994

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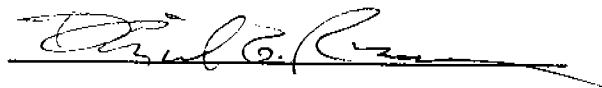
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- A. Sampling and Analytical Data
- B. Calibration Data
- C. Instrument Recorder Traces/Data Log
- D. HCOH Analysis Report (ATI)
- E. Armstrong Environmental Report
- F. Louisiana Pacific Production Summaries

REPORT CERTIFICATION

I certify that I have examined the information submitted herein, and based upon my inquiries of those directly responsible for obtaining the data or upon my direct acquisition of the data, I believe the submitted information is true, accurate and complete.

Signed



Daniel G. Russell

1.0 TEST RESULTS: The following tables present the measured flow parameters and test results for emissions and inlet loading testing for Louisiana Pacific Corporation's Urania, Louisiana MDF facility during the period January 18 through 21, 1994.

1.1 MDF Dryers RTO

1.1.1 MDF Dryers North RTO

1.1.1.1 MDF Dryers North RTO - PM/NOx/CO Emissions Test on January 18, 1994

Run No.....		1	2	3	avg.
Date		1-18-94	1-18-94	1-18-94	—
Time Start		1115	1500	1657	—
Time End		1218	1602	1802	—
PARTICULATE EMISSIONS	#/hr.	7.04	10.02	6.73	7.93
PARTICULATE EMISSIONS	gr/dscf	0.011	0.016	0.010	0.012
NOx EMISSIONS	#/hr	16.28	15.24	12.19	14.57
NOx EMISSIONS	ppm	30.7	28.5	22.7	27.3
CO EMISSIONS	#/hr	1.65	1.21	0.43	1.10
CO EMISSIONS	ppm	5.1	3.7	1.3	3.4
VOLUMETRIC FLOWRATE	acfm	99602	101518	100968	100696
VOLUMETRIC FLOWRATE	dscfm	74261	74912	75189	74787
VELOCITY	ft./sec.	41.6	42.4	42.2	42.1
STACK TEMPERATURE	° F	215	217	210	214
MOISTURE	%	5.67	6.36	6.52	6.18
SAMPLE RATE	% isokinetic	97	95	94	95

1.1.1.2 MDF Dryers North RTO - VOC/HCOH Emissions Test January 19, 1994

Run No.....		1	2	3	avg.
Date		1-19-94	1-19-94	1-19-94	-----
Time Start		1106	1627	1814	---
Time End		1506	1729	1915	---
VOC EMISSIONS	#/hr. as carbon	0.25	0.22	0.20	0.22
VOC EMISSIONS	ppm as carbon	5.8	5.5	4.8	5.4
HCOH EMISSIONS	#/hr	0.44	0.37	0.41	0.41
HCOH EMISSIONS	ppm	1.26	1.09	1.23	1.19
VOLUMETRIC FLOWRATE	acfm	101656	101619	101570	101615
VOLUMETRIC FLOWRATE	dscfm	74500	71772	71818	72697
VELOCITY	ft./sec.	42.5	42.5	42.5	42.5
STACK TEMPERATURE	° F	219	227	227	224
MOISTURE	%	6.80	9.10	9.04	8.32
SAMPLE RATE	% isokinetic	99	102	101	101

1.1.2 MDF DRYERS SOUTH RTO

1.1.2.1 MDF Dryers South RTO - PM/NOx/CO Emissions Test on January 18, 1994

Outlet sampling at the MDF Dryers South RTO was performed by Armstrong Environmental, Inc. of Dallas, Texas. A summary of results is presented in the following table. Details of the testing is provided in Armstrong Environmental's report which is reproduced in this report's Appendix E.

Run No.....		1	2	3	avg.
Date		1-18-94	1-18-94	1-18-94	—
Time Start		1114	1458	1655	—
Time End		1218	1559	1755	—
PARTICULATE EMISSIONS	#/hr.	6.37	11.69	6.80	8.29
PARTICULATE EMISSIONS	gr/dscf	0.009	0.018	0.010	0.012
NOx EMISSIONS	#/hr	16.8	15.7	13.1	15.2
NOx EMISSIONS	ppm as carbon	29.2	28.7	23.7	27.2
CO EMISSIONS	#/hr	0.32	N/D*	N/D*	0.11
CO EMISSIONS	ppm	< 1	N/D*	N/D*	< 1
VOLUMETRIC FLOWRATE	acfm	108362	105251	105071	106228
VOLUMETRIC FLOWRATE	dscfm	80061	76576	76971	77869
VELOCITY	ft./sec.	46.4	45.0	45.0	45.5
STACK TEMPERATURE	° F	220	226	221	222
MOISTURE	%	6.02	6.96	6.64	6.54
SAMPLE RATE	% isokinetic	97	98	99	98

*ND means non detected. Where calculations were made with non-detected values, a value of zero was used.

1.1.2.2 MDF Dryers South RTO - VOC/HCOH Emissions Test January 19, 1994

Outlet sampling at the MDF Dryers South RTO was performed by Armstrong Environmental, Inc. of Dallas, Texas. A summary of results is presented in the following table. Details of the testing is provided in Armstrong Environmental's report which is reproduced in this report's Appendix E.

Run No.....		1	2	3	avg.
Date		1-19-94	1-19-94	1-19-94	-----
Time Start		1106	1627	1810	---
Time End		1206	1727	1910	---
VOC EMISSIONS	#/hr. as carbon	0.25	N/D	N/D	0.08
VOC EMISSIONS	ppm as carbon	1.5	N/D	N/D	0.5
HCOH EMISSIONS	#/hr	2.47	2.96	4.40	3.28
HCOH EMISSIONS	ppm	0.95	1.15	1.60	1.23
VOLUMETRIC FLOWRATE	acfm	110535	110969	113749	111751
VOLUMETRIC FLOWRATE	dscfm	81581	80954	83207	81914
VELOCITY	ft./sec.	47.3	47.5	48.7	47.8
STACK TEMPERATURE	° F	219	226	225	217
MOISTURE	%	6.91	6.99	6.83	6.91
SAMPLE RATE	% isokinetic	98	98	102	99

1.1.3 MDF Dryers RTO Inlet

1.1.3.1 MDF Dryers RTO Inlet Loading Test for PM/CO/NO_x on January 18, 1994.

Run No.....		1	2	3	avg.
Date		1-18-94	1-18-94	1-18-94	-----
Time Start		1114	1459	1656	---
Time End		1223	1607	1809	---
PARTICULATE LOADING	#/hr.	41.33	170.45	50.63	87.47
PARTICULATE LOADING	gr/dscf	0.030	0.116	0.035	0.060
NO _x LOADING	#/hr	22.68	23.42	36.71	27.60
NO _x LOADING	ppm	19.8	19.2	30.8	23.3
CO LOADING	#/hr	7.91	11.18	9.10	9.40
CO LOADING	ppm	11.3	15.0	12.5	12.9
VOLUMETRIC FLOWRATE	acfm	185042	198324	193776	192381
VOLUMETRIC FLOWRATE	dscfm	160446	170814	166933	166065
VELOCITY	ft./sec.	32.8	35.2	34.4	34.1
STACK TEMPERATURE	° F	118	117	118	118
MOISTURE	%	5.83	6.47	6.42	6.24
SAMPLE RATE	% isokinetic	102	104	99	102

1.1.3.2 MDF Dryers RTO Inlet Loading Test for VOC and HCOH on January 19, 1994

Run No.....		1	2	3	avg.
Date		1-19-94	1-19-94	1-19-94	—
Time Start		1105	1626	1812	—
Time End		1511	1737	1921	—
VOC LOADING	#/hr. as carbon	20.08	15.40	15.83	17.10
VOC LOADING	ppm as carbon	213.0	154.6	162.5	176.7
HCOH LOADING	#/hr	4.66	6.26	7.39	6.11
HCOH LOADING	ppm	6.22	7.84	9.47	7.84
VOLUMETRIC FLOWRATE	acfm	185042	198324	193776	192381
VOLUMETRIC FLOWRATE	dscfm	160446	170814	166933	166065
VELOCITY	ft./sec.	32.8	35.2	34.4	34.1
STACK TEMPERATURE	° F	118	117	118	118
MOISTURE	%	5.83	6.47	6.42	6.24
SAMPLE RATE	% isokinetic	102	104	99	102

1.2 Press Vent

1.2.1 Press Vent RTO Outlet

1.2.1.1 Press Vent RTO Outlet Emissions Test for PM/CO/NOx on January 21, 1994.

Run No.....		1	2	3	avg.
Date		1-21-94	1-21-94	1-21-94	——
Time Start		0818	1001	1226	——
Time End		0921	1102	1327	——
PARTICULATE EMISSIONS	#/hr.	0.41	0.20	0.44	0.35
PARTICULATE EMISSIONS	gr/dscf	0.0007	0.0003	0.0007	0.0006
NOx EMISSIONS	#/hr	4.77	4.37	4.62	4.58
NOx EMISSIONS	ppm	9.4	8.3	8.8	8.8
CO EMISSIONS	#/hr	0.96	0.64	0.67	0.76
CO EMISSIONS	ppm	3.1	2.0	2.1	2.4
VOLUMETRIC FLOWRATE	acfm	88009	92058	93392	91153
VOLUMETRIC FLOWRATE	dscfm	71036	73709	73477	72741
VELOCITY	ft./sec.	62.7	65.6	66.5	64.9
STACK TEMPERATURE	° F	194	198	208	200
MOISTURE	%	1.21	1.40	1.63	1.41
SAMPLE RATE	% isokinetic	98	93	94	95

1.2.1.2 Press Vent RTO Outlet Emissions Test for VOC/HCOH on January 20, 1994.

Run No.....		1	2	3	avg.
Date		1-20-94	1-20-94	1-20-94	—
Time Start		1141	1400	1600	—
Time End		1243	1501	1703	—
VOC EMISSIONS	#/hr. as carbon	0.045	0.069	0.055	0.056
VOC EMISSIONS	ppm as carbon	1.01	1.31	1.22	1.18
HCOH EMISSIONS	#/hr	0.114	0.077	0.058	0.083
HCOH EMISSIONS	ppm	0.34	0.19	0.17	0.13
VOLUMETRIC FLOWRATE	acfm	92812	110916	93747	99159
VOLUMETRIC FLOWRATE	dscfm	72553	85938	73372	77288
VELOCITY	ft./sec.	66.1	79.0	66.8	70.6
STACK TEMPERATURE	° F	211	216	211	213
MOISTURE	%	1.69	1.89	1.64	1.74
SAMPLE RATE	% isokinetic	93	94	92	93

1.2.2 Press Vent RTO Inlet

1.2.2.1 Press Vent RTO Inlet Loading Test for PM/CO/NOx on January 21, 1994

Run No.....		1	2	3	avg.
Date		1-21-94	1-21-94	1-21-94	-----
Time Start		0817	1000	1225	---
Time End		0920	1101	1226	---
PARTICULATE LOADING	#/hr.	2.59	2.91	2.83	2.78
PARTICULATE LOADING	gr/dscf	0.005	0.005	0.005	0.005
NOx LOADING	#/hr	N/D	N/D	N/D	N/D
NOx LOADING	ppm	N/D	N/D	N/D	N/D
CO LOADING	#/hr	N/D	N/D	N/D	N/D
CO LOADING	ppm	N/D	N/D	N/D	N/D
VOLUMETRIC FLOWRATE	acfm	66946	68931	69475	68450
VOLUMETRIC FLOWRATE	dscfm	64908	66822	65706	65812
VELOCITY	ft./sec.	47.3	48.7	49.1	48.4
STACK TEMPERATURE	° F	81	83	96	87
MOISTURE	%	1.25	0.91	1.15	1.10
SAMPLE RATE	% isokinetic	95	93	93	94

1.2.2.2 Press Vent RTO Inlet Loading Test for VOC/HCOH on January 20, 1994

Run No.....		1	2	3	avg.
Date		1-20-94	1-20-94	1-20-94	-----
Time Start		1140	1359	1559	-----
Time End		1242	1500	1701	-----
VOC LOADING	#/hr. as carbon	0.78	0.71	0.84	0.78
VOC LOADING	ppm as carbon	19.0	15.1	20.6	18.2
HCOH LOADING	#/hr	11.73	10.11	8.24	10.03
HCOH LOADING	ppm	37.73	28.33	26.79	30.95
VOLUMETRIC FLOWRATE	acfm	70878	80996	69798	73891
VOLUMETRIC FLOWRATE	dscfm	66501	76336	65819	69552
VELOCITY	ft./sec.	50.1	57.3	49.3	52.2
STACK TEMPERATURE	° F	102	98	98	99
MOISTURE	%	0.79	1.07	0.96	0.94
SAMPLE RATE	% isokinetic	99	101	99	99

1.3. Efficiency Summary: The following tabular summaries of system removal efficiencies are based on mass emission rates. Emissions expressed in the tables are in pounds per hour.

1.3.1. MDF Dryers RTO

	PM	VOC	HCOH	CO	NOx
NORTH RTO	7.93	0.22	0.41	1.10	14.6
SOUTH RTO	8.29	0.08	0.47	0.0	15.2
OUTLET TOTAL	16.22	0.30	0.88	1.10	29.8
INLET	87.5	17.1	6.11	9.4	27.6
REMOVAL %	81.46	98.3	85.6	88.30	-7.97

1.3.2. Press Vent RTO

	PM	VOC	HCOH	CO	NOx
OUTLET	0.35	0.056	0.08	0.76	4.58
INLET	2.78	0.776	10.03	ND*	ND*
REMOVAL %	87.41	92.78	99.20	N/A	N/A

* ND means non detected.

2.0 SOURCE DESCRIPTION: Louisiana Pacific Corporation operates a Medium Density Fiberboard (MDF) plant at its wood products complex in Urania, Louisiana. Two emissions producing processes associated with the manufacture of MDF are the drying of wood fiber and ventilation of the press. Process description here is limited to a brief description of the emissions sources and their sampling locations. Detailed descriptions of the processes, the pollution control equipment, and records of operating rates and conditions may be supplied by Louisiana Pacific Corporation.

L.P.'s MDF plant utilizes two direct heat wood fired dryers. The two dryers each have two exhausts and each exhaust is directed to primary cyclones. The exhausts from the four cyclones are combined to a common header preceding introduction to the emissions control equipment. Two Smith Engineering Company regenerative thermal oxidizers (RTO) have been installed for control of emissions from the dryers. The single header from the dryers enters a mixing box which acts as a settling chamber and air mixer. From the mixing box, the air is directed to and split equally between the twin RTO's designated as North RTO and South RTO. The selected inlet sampling location is in the header location immediately preceding the mixing box. This sampling location is not ideal but is the only location where air quality entering the RTO's can be determined. The ducts leaving the four cyclones combine into a common circular horizontal duct. The circular horizontal duct makes a 90° transition to a rectangular arch duct which enters the top of the mixing box. The rectangular arch is 144 inches wide by 94 inches deep and has an 11 foot center radius. As expected, most of the air was moving along the outside of the arch. Though the flow was not evenly distributed across the sampling traverses, air movement was laminar as verified by a null pitot technique. The RTO's exhaust to the atmosphere by way of 85.5 inch diameter vertical stacks. For each, two sample ports are provided at a location which is 44 inches (0.5 diameters) below the stack exit, and 229 inches (2.68 diameters) above the duct to stack transition. Sketches of the stacks and sampling locations are provided in Appendix A.

Emissions from the continuous press are also controlled by a Smith Engineering Company RTO. The press area is enclosed and ducted to the RTO in such a manner that any openings in the enclosure have inward velocities of greater than 200 feet per minute. The sampling location for the inlet to the press vent RTO is a vertical turned downward section of 65.75 inch diameter duct. Two sampling ports at 90° are provided at a location which is 148 inches (2.2 diameters) downstream of a horizontal to vertical elbow and 62 inches (0.9 diameters) above a vertical to horizontal elbow. The RTO exhausts to the atmosphere by way of a 65.50 inch vertical stack. Two sample ports at 90° are provided at a location which is 72 inches (1.1 diameters) below the stack exit and 204 inches (3.1 diameters) above the system inlet duct to stack transition. Sketches of the stacks and sampling locations are provided in Appendix A.

3.0 TEST PROCEDURES: Test procedures used are those described in 40 CFR, Part 60, Appendix A and in Part 266, Appendix IX..

Particulate sampling was done as described in Method 5. An exception was the inclusion of the condenser section particulate as described in Method 202. Reported particulate is based on three fractions: the front half, the back half organic (methylene chloride extraction), and the back half aqueous. The contribution of each fraction can be reviewed in Section 4.0.

Carbon monoxide concentrations were continuously monitored as described in Method 10. A Beckman Model 864 NDIR with a 0 to 1000 ppm range was used for inlet locations. Outlet concentrations were monitored using a TECO Model 48H gas correlation filter NDIR in various ranges. The exhausts of the CO instruments were captured in Tedlar bags in order to obtain an integrated gas sample. Oxygen content of the bag samples was measured using a calibrated Servomex paramagnetic oxygen analyzer. Carbon dioxide was measured using an Orsat analyzer. Instrument calibration was performed prior to and following each series of tests, and a mid range system bias check was made prior to and following each run by directing calibration to the gas sampling probe.

Nitrogen oxides were continuously monitored as described in Method 7E. Two TECO Model 10S analyzers were used. Instrument calibration was performed prior to and following each series of tests, and a mid range system bias check was made prior to and following each run by directing calibration to the gas sampling probe.

VOC concentrations were measured using Method 25A (continuous monitoring with a flame ionization detector). A TECO Model 51 was used at the outlet locations and a Ratfish Model 55CA was used at the inlet locations. Both FIDs are equipped with multiple scales. The 0 to 100 ppm scale and the 0 to 1000 ppm scale were used for calibrations using zero air, and appropriate low, mid and high range concentrations of EPA protocol propane in nitrogen. Since calibrations are made with propane (C_3H_8), results as methane (CH_4) (or as carbon) are determined by increasing the measured concentration by a factor of three. A continuous trace of VOC as propane was recorded and manually integrated for each 60 minute test period. Instrument calibration was performed initially, and following each 60 minute test period. Any necessary adjustments were made after recording the response of the mid range calibration gas, which was introduced at the inlet to the VOC sampling probe. The gas samples were directed to the heated FID analyzers by way of heated teflon sample lines maintained at a minimum temperature of 275°F.

Formaldehyde was measured using the procedure described in CFR 40, Part 266, Appendix IX, Method 0011. Reagent preparation and sample analysis was performed by Air Techniques and Oxford Laboratories of Marietta, Georgia.

Inlet sampling was done simultaneously with outlet sampling in order to determine removal efficiency or additional pollutant contribution. For the dryers, this required the operation of three sample trains simultaneously at relatively far removed locations. Armstrong Engineering of Dallas, Texas, performed the outlet sampling at the South RTO outlet. A report of that testing is provided in Appendix E of this report.

4.0 DATA REDUCTION

LP - Urania
MDF Dryers North RTO
PM/CO/NOx Emissions Test - January 18, 1994

Collected Test Data:

		RUN 1	RUN 2	RUN 3
Date	:	1/18/94	1/18/94	1/18/94
Time	:	1115	1500	1657
Time end	:	1218	1602	1802
1. As	: sq ft	39.87123	39.87123	39.87123
2. Dn	: in.	0.242	0.305	0.305
3. Cp	: dimensionless	0.84	0.84	0.84
4. Theta	: minutes	60.00	60.00	60.00
5. Y	: dimensionless	1.01	1.01	1.01
6. Pbar	: in. Hg	30.25	30.25	30.25
7. Pg	: in. H2O	-0.36	-0.36	-0.36
8. Vm	: cf (dry gas)	35.361	56.451	56.426
9. $\text{sqr}(\text{DP})_{\text{avg}}$	: in.H2O ^{0.5}	0.6531	0.6636	0.6634
10. DH	: in. H2O	1.0400	2.8917	2.9646
11. ts	: degrees F	214.79	216.83	209.50
12. tm	: degrees F	94.85	106.83	107.90
13. Vlc	: ml	44	78	80
14. CO2	: percent	1.00	0.90	0.90
15. O2	: percent	19.80	19.80	19.80
16. CO	: percent	0	0	0
17. CO	: ppm	5.1	3.7	1.3
18. M,PM	: milligrams			
	front half	21.8	51.1	32.8
	back half organic	0.1	1.5	1.6
	back half aqueous	2.8	2.1	2.1
20. NOx	: ppm	30.7	28.5	22.7

213.71

3.4

27.3

LP - Urania

MDF Dryers North RTO

PM/CO/NOx Emissions Test - January 18, 1994

Calculations:

		RUN 1	RUN 2	RUN 3	AVG.
1. Pm	: in.Hg (DH/13.6)+Pbar	30.3265	30.4626	30.4680	
2. Ps	: in. Hg (Pg/13.6)+Pbar	30.2235	30.2235	30.2235	
3. An	: sq ft $((Dn/24)^2)(3.1416)$	3.19E-04	5.07E-04	5.07E-04	
4. Vmstd	: dscf $Vm Y(Pm/Pstd)(Tstd/Tm)$	34.448	54.073	53.957	47.493
5. Vwstd	: scf $(.04707cf/m)(Vic)$	2.071	3.671	3.766	
6. Bws	: dimensionless $Vwstd/(Vwstd+Vmstd)$	0.0567	0.0636	0.0652	0.0618
7. Md	: mol.wt. dry basis .44 CO2+.32 O2+.28(CO+N2)	28.952	28.936	28.936	
8. Ms	: mol.wt. wet basis $Md(1-Bws)+18 Bws$	28.33	28.24	28.22	
9. Vs	: ft/sec $Kp Cp (sqrDP)sqr(Ts/(Ps Ms))$	41.63	42.44	42.21	42.09
10. Q	: cfm $Vs As(60 \text{ sec/min})$	99602	101518	100968	100696
11. Qstw	: scfm $Q(Ps/Pstd)(Tstd/Ts)$	78726	79998	80436	79720
12. Qstd	: dscfm $Qstw(1-Bws)$	74261	74912	75189	74787
13. I	: percent $[(100 Ts)(.002669 Vic+(Vm Pm/Tm))/(60 \text{ theta Vs Ps An})]$	96.51	94.54	93.99	95.01

Particulate Emissions

14. E,PM	: pounds/hr $(M,PM/Vmstd)(Qstd)(60)/(453590)$				
front half		6.216	9.364	6.046	7.209
back half organic		0.029	0.275	0.295	0.199
back half aqueous		0.798	0.385	0.387	0.523
Total		7.043	10.024	6.728	7.932
15. C,PM	: grains/dscf $(M,PM/Vmstd)(.0154 \text{ grains/mg})$				
front half		0.010	0.015	0.009	0.011
back half organic		0.000	0.000	0.000	0.000
back half aqueous		0.001	0.001	0.001	0.001
Total		0.011	0.016	0.010	0.012

Carbon Monoxide Emissions

16. E,CO	: pounds/hr. $(C,CO)(7.27e-8)(Qstd)(60)$	1.652	1.209	0.426	1.096
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NOx Emissions

17. E,NOx	: pounds/hr. $(C,NOx)(1.19e-7)(Qstd)(60)$	16.278	15.244	12.186	14.569
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LP - Urania

MDF Dryers RTO Inlet

PM/CO/NOx Loading Test - January 18, 1994

Collected Test Data:

		RUN 1	RUN 2	RUN 3	
Date	:	1/18/94	1/18/94	1/18/94	
Time	:	1114	1459	1656	
Time end	:	1223	1607	1809	
1. As	: sq ft	94	94	94	
2. Dn	: in.	0.272	0.272	0.272	
3. Cp	: dimensionless	0.84	0.84	0.84	
4. Theta	: minutes	62.50	62.50	62.50	
5. Y	: dimensionless	1.00	1.00	1.00	
6. Pbar	: in. Hg	30.25	30.25	30.25	
7. Pg	: in. H2O	-1.6	-1.6	-1.6	
8. Vm	: cf (dry gas)	46.052	49.943	46.843	
9. sqr(DP),avg	: in.H2O^.5	0.5553	0.5945	0.5808	
10. DH	: in. H2O	2.1603	2.3128	2.2436	
11. ts	: degrees F	117.52	117.44	117.60	117.52
12. tm	: degrees F	100.20	102.90	108.52	
13. Vlc	: ml	58	70	64.5	
14. CO2	: percent	1.00	1.00	1.00	
15. O2	: percent	19.80	19.90	19.80	
16. CO	: percent	0	0	0	
17. CO	: ppm	11.3	15.0	12.5	12.9
18. M,PM	: milligrams				
	front half	81.3	351.1	90.4	
	back half organic	2.7	5.2	5.5	
	back half aqueous	1.9	3	5.5	
19. NOx	: ppm	19.8	19.2	30.8	23.3

LP - Urania

MDF Dryers RTO Inlet

PM/CO/NOx Loading Test - January 18, 1994

Calculations:		RUN 1	RUN 2	RUN 3	AVG.
1. Pm	: in.Hg (DH/13.6)+Pbar	30.4088	30.4201	30.4150	
2. Ps	: in. Hg (Pg/13.6)+Pbar	30.1324	30.1324	30.1324	
3. An	: sq ft ((Dn/24)^2)(3.1416)	4.04E-04	4.04E-04	4.04E-04	
4. Vmstd	: dscf Vm Y(Pm/Pstd)(Tstd/Tm)	44.114	47.629	44.224	45.323
5. Vwstd	: scf (.04707cf/ml)(Vlc)	2.730	3.295	3.036	
6. Bws	: dimensionless Vwstd/(Vwstd+Vmstd)	0.0583	0.0647	0.0642	0.0624
7. Md	: mol.wt. dry basis .44 CO2+.32 O2+.28(CO+N2)	28.952	28.956	28.952	
8. Ms	: mol.wt. wet basis Md(1-Bws)+18 Bws	28.31	28.25	28.25	
9. Vs	: ft/sec Kp Cp (sqrDP)sqr(Ts/(Ps Ms))	32.81	35.16	34.36	34.11
10. Q	: cfm Vs As(60 sec/min)	185042	198324	193776	192381
11. Qstw	: scfm Q(Ps/Pstd)(Tstd/Ts)	170376	182631	178393	177133
12. Qstd	: dscfm Qstw(1-Bws)	160446	170814	166933	166065
13. I	: percent ((100 Ts)(.002669 Vlc+(Vm Pm/Tm))/(60 theta Vs Ps An)	102.48	103.93	98.75	101.72

Particulate Emissions

14. E,PM	: pounds/hr (M,PM/Vmstd)(Qstd)(60)/(453590)				
front half		39.114	166.558	45.138	83.603
back half organic		1.299	2.467	2.746	2.171
back half aqueous		0.914	1.423	2.746	1.694
Total		41.327	170.448	50.630	87.469
15. C,PM	: grains/dscf (M,PM/Vmstd)(.0154 grains/mg)				
front half		0.028	0.114	0.031	0.058
back half organic		0.001	0.002	0.002	0.002
back half aqueous		0.001	0.001	0.002	0.001
Total		0.030	0.116	0.035	0.060

Carbon Monoxide Emissions

22. E,CO	: pounds/hr. (C,CO)(7.27e-8)(Qstd)(60)	7.909	11.176	9.102	9.396
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NOx Emissions

23. E,NOx	: pounds/hr. (C,NOx)(1.19e-7)(Qstd)(60)	22.683	23.417	36.711	27.603
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LP - Urania
MDF Dryers North RTO
VOC/HCOH Emissions Test - January 19, 1994

Collected Test Data:

		RUN 1	RUN 2	RUN 3
Date	:	1/19/94	1/19/94	1/19/94
Time	:	1106	1627	1814
Time end	:	1506	1729	1915
1. As	: sq ft	39.87123	39.87123	39.87123
2. Dn	: in.	0.277	0.277	0.277
3. Cp	: dimensionless	0.84	0.84	0.84
4. Theta	: minutes	60.00	60.00	60.00
5. Y	: dimensionless	1.01	1.01	1.01
6. Pbar	: in. Hg	30.28	30.28	30.28
7. Pg	: in. H2O	-0.36	-0.36	-0.36
8. Vm	: cf (dry gas)	46.64	48.062	47.705
9. sqr(DP),avg	: in.H2O ^{0.5}	0.6634	0.6561	0.6560
10. DH	: in. H2O	2.1396	2.0833	2.1021
11. ts	: degrees F	218.96	227.08	226.79
12. tm	: degrees F	84.63	103.25	109.23
13. Vlc	: ml	72	98.5	96
14. CO2	: percent	1.00	0.90	0.90
15. O2	: percent	19.80	19.80	19.80
16. CO	: percent	0	0	0
17. C,VOC	: ppm as propane, wet basis	1.80	1.65	1.47
20. M,HCOH	: micrograms	2070	1790	1970

224.28

1.64

LP - Urania

MDF Dryers North RTO

VOC/HCOH Emissions Test - January 19, 1994

Calculations:

		RUN 1	RUN 2	RUN 3	AVG.
1. Pm	: in.Hg (DH/13.6)+Pbar	30.4373	30.4332	30.4346	
2. Ps	: in. Hg (Pg/13.6)+Pbar	30.2535	30.2535	30.2535	
3. An	: sq ft ((Dn/24)^2)(3.1416)	4.18E-04	4.18E-04	4.18E-04	
4. Vmstd	: dscf Vm Y(Pm/Pstd)(Tstd/Tm)	46.458	46.285	45.461	46.068
5. Vwstd	: scf (.04707cf/ml)(Vic)	3.389	4.636	4.519	
6. Bws	: dimensionless Vwstd/(Vwstd+Vmstd)	0.0680	0.0910	0.0904	0.0832
7. Md	: mol.wt. dry basis .44 CO2+.32 O2+.28(CO+N2)	28.952	28.936	28.936	
8. Ms	: mol.wt. wet basis Md(1-Bws)+18 Bws	28.21	27.94	27.95	
9. Vs	: ft/sec Kp Cp (sqrDP)sqr(Ts/(Ps Ms))	42.49	42.48	42.46	42.48
10. Q	: cfm Vs As(60 sec/min)	101656	101619	101570	101615
11. Qstw	: scfm Q(Ps/Pstd)(Tstd/Ts)	79935	78962	78957	79284
12. Qstd	: dscfm Qstw(1-Bws)	74500	71772	71818	72697
13. I	: percent (((100 Ts)(.002669 Vic+(Vm Pm/Tm)))/(60 theta Vs Ps An)	99.02	102.41	100.52	100.65

VOC Emissions

14. CVOC	: ppm as C,dry basis ((C,VOC)(3))/(1-bws)	5.79	5.45	4.84	5.36
15. E,VOC	: pounds/hr. (CVOC)(3.12e-8)(Qstd)(60)	0.251	0.222	0.197	0.223

HCOH Emissions

16. C,HCOH	: ppm (M,HCOH/Vmstd)(.0283)	1.261	1.094	1.226	1.194
17. E,HCOH	: pounds/hr. (M,HCOH/Vmstd)(Qstd)(60)/(453590000)	0.439	0.367	0.412	0.406

LP - Urania

MDF Dryers RTO Inlet

VOC/HCOH Loading Test - January 19, 1994

Collected Test Data:

		RUN 1	RUN 2	RUN 3
Date		1/19/94	1/19/94	1/19/94
Time		1105	1626	1812
Time end		1511	1737	1921
1. As	: sq ft	94	94	94
2. Dn	: in.	0.272	0.272	0.272
3. Cp	: dimensionless	0.84	0.84	0.84
4. Theta	: minutes	62.50	62.50	62.50
5. Y	: dimensionless	1.00	1.00	1.00
6. Pbar	: in. Hg	30.25	30.25	30.25
7. Pg	: in. H2O	-1.6	-1.6	-1.6
8. Vm	: cf (dry gas)	46.052	49.943	46.843
9. sqr(DP),avg	: in.H2O^.5	0.5553	0.5945	0.5808
10. DH	: in. H2O	2.1603	2.3128	2.2436
11. ts	: degrees F	117.52	117.44	117.60
12. tm	: degrees F	100.20	102.90	108.52
13. Vlc	: ml	58	70	64.5
14. CO2	: percent	1.00	1.00	1.00
15. O2	: percent	19.80	19.90	19.80
16. CO	: percent	0	0	0
17. C,VOC	: ppm as propane, wet basis	66.86	48.19	50.68
18. M,HCOH	: micrograms	9690	13200	14800

117.52

55.24

LP - Urania

MDF Dryers RTO Inlet

VOC/HCOH Loading Test - January 19, 1994

Calculations:

		RUN 1	RUN 2	RUN 3	AVG.
1. Pm	: in.Hg (DH/13.6)+Pbar	30.4088	30.4201	30.4150	
2. Ps	: in. Hg (Pg/13.6)+Pbar	30.1324	30.1324	30.1324	
3. An	: sq ft ((Dn/24)^2)(3.1416)	4.04E-04	4.04E-04	4.04E-04	
4. Vmstd	: dscf Vm Y(Pm/Pstd)(Tstd/Tm)	44.114	47.629	44.224	45.323
5. Vwstd	: scf (.04707cf/ml)(Vic)	2.730	3.295	3.036	
6. Bws	: dimensionless Vwstd/(Vwstd+Vmstd)	0.0583	0.0647	0.0642	0.0624
7. Md	: mol.wt. dry basis .44 CO2+.32 O2+.28(CO+N2)	28.952	28.956	28.952	
8. Ms	: mol.wt. wet basis Md(1-Bws)+18 Bws	28.31	28.25	28.25	
9. Vs	: ft/sec Kp Cp (sqrDP)sqr(Ts/(Ps Ms))	32.81	35.16	34.36	34.11
10. Q	: cfm Vs As(60 sec/min)	185042	198324	193776	192381
11. Qstw	: scfm Q(Ps/Pstd)(Tstd/Ts)	170376	182631	178393	177133
12. Qstd	: dscfm Qstw(1-Bws)	160446	170814	166933	166065
13. I	: percent [(100 Ts)(.002669 Vic+(Vm Pm/Tm))/(60 theta Vs Ps An)	102.48	103.93	98.75	101.72

VOC Loading

14. CVOC	: ppm as C,dry basis ((C,VOC)(3))/(1-bws)	212.99	154.57	162.48	176.68
15. E,VOC	: pounds/hr. (CVOC)(3.12e-8)(Qstd)(60)	20.075	15.404	15.832	17.104

HCOH Loading

16. C,HCOH	: ppm (M,HCOH/Vmstd)(.0283)	6.216	7.843	9.471	7.843
17. E,HCOH	: pounds/hr. (M,HCOH/Vmstd)(Qstd)(60)/(453590000)	4.662	6.262	7.390	6.105

LP - Urania
MDF Press Vent RTO
PM/CO/NOx Emissions Test - January 21, 1994

Collected Test Data:

		RUN 1	RUN 2	RUN 3	
Date	:	1/21/94	1/21/94	1/21/94	
Time	:	0818	1001	1226	
Time end	:	0921	1102	1327	
1. As	: sq ft	23.39968	23.39968	23.39968	
2. Dn	: in.	0.266	0.266	0.266	
3. Cp	: dimensionless	0.84	0.84	0.84	
4. Theta	: minutes	60.00	60.00	60.00	
5. Y	: dimensionless	1.01	1.01	1.01	
6. Pbar	: in. Hg	30.31	30.31	30.31	
7. Pg	: in. H2O	-0.5	-0.5	-0.5	
8. Vm	: cf (dry gas)	69.964	70.104	71.120	
9. sqr(DP),avg	: in.H2O ^{0.5}	1.0063	1.0490	1.0557	
10. DH	: in. H2O	4.8333	4.7250	4.8542	
11. ts	: degrees F	193.88	197.92	207.96	199.92
12. tm	: degrees F	92.58	101.79	110.00	
13. Vlc	: ml	18	20.5	24	
14. CO2	: percent	0.00	0.00	0.00	
15. O2	: percent	20.90	20.90	20.90	
16. CO	: percent	0	0	0	
17. CO	: ppm	3.1	2.0	2.1	2.4
18. M,PM	: milligrams				
	front half	2.6	0.3	1.6	
	back half organic	0.1	0.9	0.7	
	back half aqueous	0.3	0.2	0.8	
19. NOx	: ppm	9.4	8.3	8.8	8.8

LP - Urania

MDF Press Vent RTO

PM/CO/NOx Emissions Test - January 21, 1994

Calculations:

		RUN 1	RUN 2	RUN 3	AVG.
1. Pm	: in.Hg (DH/13.6)+Pbar	30.6654	30.6574	30.6669	
2. Ps	: in. Hg (Pg/13.6)+Pbar	30.2732	30.2732	30.2732	
3. An	: sq ft ((Dn/24)^2)(3.1416)	3.86E-04	3.86E-04	3.86E-04	
4. Vmstd	: dscf Vm Y (Pm/Pstd)(Tstd/Tm)	69.202	68.186	68.199	68.529
5. Vwstd	: scf (.04707cf/ml)(Vlc)	0.847	0.965	1.130	
6. Bws	: dimensionless Vwstd/(Vwstd+Vmstd)	0.0121	0.0140	0.0163	0.0141
7. Md	: mol.wt. dry basis .44 CO2+.32 O2+.28(CO+N2)	28.836	28.836	28.836	
8. Ms	: mol.wt. wet basis Md(1-Bws)+18 Bws	28.70	28.68	28.66	
9. Vs	: ft/sec Kp Cp (sqrDP)sqr(Ts/(Ps Ms))	62.69	65.57	66.52	64.92
10. Q	: cfm Vs As(60 sec/min)	88009	92058	93392	91153
11. Qstw	: scfm Q(Ps/Pstd)(Tstd/Ts)	71905	74752	74695	73784
12. Qstd	: dscfm Qstw(1-Bws)	71036	73709	73477	72741
13. I	: percent [(100 Ts)(.002669 Vlc+(Vm Pm/Tm))/(60 theta Vs Ps An)]	98.45	93.49	93.80	95.25

Particulate Emissions

14. E,PM	: pounds/hr (M,PM/Vmstd)(Qstd)(60)/(453590)				
front half		0.353	0.043	0.228	0.208
back half organic		0.014	0.129	0.100	0.081
back half aqueous		0.041	0.029	0.114	0.061
Total		0.407	0.200	0.442	0.350
15. C,PM	: grains/dscf (M,PM/Vmstd)(.0154 grains/mg)				
front half		0.0006	0.0001	0.0004	0.0003
back half organic		0.0000	0.0002	0.0002	0.0001
back half aqueous		0.0001	0.0000	0.0002	0.0001
Total		0.0007	0.0003	0.0007	0.0006

Carbon Monoxide Emissions

16. E,CO	: pounds/hr. (C,CO)(7.27e-8)(Qstd)(60)	0.961	0.643	0.673	0.759
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NOx Emissions

17. E,NOx	: pounds/hr. (C,NOx)(1.19e-7)(Qstd)(60)	4.768	4.368	4.617	4.584
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LP - Urania

MDF Press Vent RTO Inlet

PM/CO/NOx Loading Test - January 21, 1994

Collected Test Data:

		RUN 1	RUN 2	RUN 3
Date		1/21/94	1/21/94	1/21/94
Time		0817	1000	1225
Time end		0920	1101	1226
1. As	: sq ft	23.57865	23.57865	23.57865
2. Dn	: in.	0.218	0.218	0.218
3. Cp	: dimensionless	0.84	0.84	0.84
4. Theta	: minutes	60.00	60.00	60.00
5. Y	: dimensionless	1.00	1.00	1.00
6. Pbar	: in. Hg	30.31	30.31	30.31
7. Pg	: in. H2O	-2.6	-2.6	-2.6
8. Vm	: cf (dry gas)	40.999	42.375	42.307
9. sqr(DP),avg	: in.H2O ^{0.5}	0.8327	0.8564	0.8532
10. DH	: in. H2O	1.5563	1.6688	1.6417
11. ts	: degrees F	81.33	83.29	95.54
12. tm	: degrees F	79.38	95.71	101.08
13. Vlc	: ml	11	8	10
14. CO2	: percent	0.00	0.00	0.00
15. O2	: percent	20.90	20.90	20.90
16. CO	: percent	0	0	0
17. CO	: ppm	0	0	0
18. M,PM	: milligrams			
	front half	8.3	7.3	6.3
	back half organic	2.3	3	2.9
	back half aqueous	1.7	3.2	4
19. NOx	: ppm	0	0	0

86.72

0.00

0.00

LP - Urania

MDF Press Vent RTO Inlet

PM/CO/NOx Loading Test - January 21, 1994

Calculations:

		RUN 1	RUN 2	RUN 3	AVG.
1. Pm	: in.Hg (DH/13.6)+Pbar	30.4244	30.4327	30.4307	
2. Ps	: in. Hg (Pg/13.6)+Pbar	30.1188	30.1188	30.1188	
3. An	: sq ft ((Dn/24)^2)(3.1416)	2.59E-04	2.59E-04	2.59E-04	
4. Vmstd	: dscf Vm Y (Pm/Pstd)(Tstd/Tm)	40.811	40.952	40.492	40.752
5. Vwstd	: scf (.04707cf/ml)(Vic)	0.518	0.377	0.471	
6. Bws	: dimensionless Vwstd/(Vwstd+Vmstd)	0.0125	0.0091	0.0115	0.0110
7. Md	: mol.wt. dry basis .44 CO2+.32 O2+.28(CO+N2)	28.836	28.836	28.836	
8. Ms	: mol.wt. wet basis Md(1-Bws)+18 Bws	28.70	28.74	28.71	
9. Vs	: ft/sec Kp Cp (sqrDP)sqr(Ts/(Ps Ms))	47.32	48.72	49.11	48.38
10. Q	: cfm Vs As(60 sec/min)	66946	68931	69475	68450
11. Qstwr	: scfm Q(Ps/Pstd)(Tstd/Ts)	65731	67436	66469	66546
12. Qstd	: dscfm Qstwr(1-Bws)	64908	66822	65706	65812
13. I	: percent [(100 Ts)(.002669 Vic+(Vm Pm/Tm))/(60 theta Vs Ps An)	95.33	92.91	93.43	93.89

Particulate Emissions

14. E,PM	: pounds/hr (M,PM/Vmstd)(Qstd)(60)/(453590)				
front half		1.746	1.576	1.352	1.558
back half organic		0.484	0.648	0.622	0.585
back half aqueous		0.358	0.691	0.859	0.636
Total		2.588	2.914	2.833	2.778
15. C,PM	: grains/dscf (M,PM/Vmstd)(.0154 grains/mg)				
front half		0.0031	0.0027	0.0024	0.0028
back half organic		0.0009	0.0011	0.0011	0.0010
back half aqueous		0.0006	0.0012	0.0015	0.0011
Total		0.0046	0.0051	0.0050	0.0049

Carbon Monoxide Emissions

22. E,CO	: pounds/hr. (C,CO)(7.27e-8)(Qstd)(60)	0.000	0.000	0.000	0.000
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NOx Emissions

23. E,NOx	: pounds/hr. (C,NOx)(1.19e-7)(Qstd)(60)	0.000	0.000	0.000	0.000
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LP - Urania
MDF Press Vent RTO
VOC/HCOH Emissions Test - January 20, 1994

Collected Test Data:

		RUN 1	RUN 2	RUN 3
Date		1/20/94	1/20/94	1/20/94
Time		1141	1400	1600
Time end		1243	1501	1703
1. As	: sq ft	23.39968	23.39968	23.39968
2. Dn	: in.	0.218	0.218	0.218
3. Cp	: dimensionless	0.84	0.84	0.84
4. Theta	: minutes	60.00	60.00	60.00
5. Y	: dimensionless	1.01	1.01	1.01
6. Pbar	: in. Hg	30.29	30.29	30.29
7. Pg	: in. H2O	-0.5	-0.5	-0.5
8. Vm	: cf (dry gas)	45.377	54.897	47.099
9. sqr(DP),avg	: in.H2O ^{.5}	1.0460	1.2456	1.0570
10. DH	: in. H2O	1.9583	2.8167	2.0271
11. ts	: degrees F	211.38	216.04	210.92
12. tm	: degrees F	86.38	94.60	107.31
13. Vlc	: ml	16.5	22	16
14. CO2	: percent	0.00	0.10	0.00
15. O2	: percent	20.90	20.90	20.90
16. CO	: percent	0	0	0
17. C,VOC	: ppm as propane, wet basis	0.33	0.43	0.40
20. M,HCOH	: micrograms	534	363	269

212.78

0.39

LP - Urania

MDF Press Vent RTO

VOC/HCOH Emissions Test - January 20, 1994

Calculations:

		RUN 1	RUN 2	RUN 3	AVG.
1. Pm	: in.Hg $(DH/13.6)+Pbar$	30.4340	30.4971	30.4391	
2. Ps	: in. Hg $(Pg/13.6)+Pbar$	30.2532	30.2532	30.2532	
3. An	: sq ft $((Dn/24)^2)(3.1416)$	2.59E-04	2.59E-04	2.59E-04	
4. Vmstd	: dscf $Vm Y(Pm/Pstd)(Tstd/Tm)$	45.050	53.805	45.042	47.966
5. Vwstd	: scf $(.04707cf/ml)(Vic)$	0.777	1.036	0.753	
6. Bws	: dimensionless $Vwstd/(Vwstd+Vmstd)$	0.0169	0.0189	0.0164	0.0174
7. Md	: mol.wt. dry basis .44 CO ₂ + .32 O ₂ + .28(CO+N ₂)	28.836	28.852	28.836	
8. Ms	: mol.wt. wet basis $Md(1-Bws)+18 Bws$	28.65	28.65	28.66	
9. Vs	: ft/sec $Kp Cp (sqrDP)sqr(Ts/(Ps Ms))$	66.11	79.00	66.77	70.63
10. Q	: cfm $Vs As(60 \text{ sec/min})$	92812	110916	93747	99159
11. Qstw	: scfm $Q(Ps/Pstd)(Tstd/Ts)$	73804	87592	74599	78665
12. Qstd	: dscfm $Qstw(1-Bws)$	72553	85938	73372	77288
13. I	: percent $[(100 Ts)(.002669 Vic+(Vm Pm/Tm))/(60 \text{ theta } Vs Ps An)$	93.42	94.20	92.37	93.33

VOC Emissions

14. CVOC	: ppm as C, dry basis $((C,VOC)(3))/(1-bws)$	1.01	1.31	1.22	1.18
15. E,VOC	: pounds/hr. $(CVOC)(3.12e-8)(Qstd)(60)$	0.045	0.069	0.055	0.056

HCOH Emissions

16. C,HCOH	: ppm $(M,HCOH/Vmstd)(.0283)$	0.335	0.191	0.169	0.232
17. E,HCOH	: pounds/hr. $(M,HCOH/Vmstd)(Qstd)(60)/(453590000)$	0.114	0.077	0.058	0.083

LP - Urania

MDF Press Vent RTO Inlet

VOC/HCOH Loading Test - January 20, 1994

Collected Test Data:

		RUN 1	RUN 2	RUN 3
Date		1/20/94	1/20/94	1/20/94
Time		1140	1359	1559
Time end		1242	1500	1701
1. As	: sq ft	23.57865	23.57865	23.57865
2. Dn	: in.	0.260	0.260	0.260
3. Cp	: dimensionless	0.84	0.84	0.84
4. Theta	: minutes	60.00	60.00	60.00
5. Y	: dimensionless	1.00	1.00	1.00
6. Pbar	: in. Hg	30.29	30.29	30.29
7. Pg	: in. H2O	-2.6	-2.6	-2.6
8. Vm	: cf (dry gas)	63.017	74.815	62.952
9. sqrt(DP),avg	: in.H2O^.5	0.8660	0.9927	0.8554
10. DH	: in. H2O	3.6804	5.1417	3.6000
11. ts	: degrees F	101.63	97.58	97.88
12. tm	: degrees F	89.81	101.46	96.96
13. Vlc	: ml	10.5	16.5	12.5
14. CO2	: percent	0.00	0.00	0.00
15. O2	: percent	20.90	20.90	20.90
16. CO	: percent	0	0	0
17. C,VOC	: ppm as propane, wet basis	6.28	4.97	6.80
18. M,HCOH	: micrograms	82400	72200	57700

99.03

6.02

LP - Urania

MDF Press Vent RTO Inlet

VOC/HCOH Loading Test - January 20, 1994

Calculations:

RUN 1

RUN 2

RUN 3

AVG.

1. Pm	: in.Hg				
	(DH/13.6)+Pbar	30.5606	30.6681	30.5547	
2. Ps	: in. Hg				
	(Pg/13.6)+Pbar	30.0988	30.0988	30.0988	
3. An	: sq ft				
	((Dn/24)^2)(3.1416)	3.69E-04	3.69E-04	3.69E-04	
4. Vmstd	: dscf				
	Vm Y(Pm/Pstd)(Tstd/Tm)	61.813	72.115	60.945	64.958
5. Vwstd	: scf				
	(.04707cf/ml)(Vic)	0.494	0.777	0.588	
6. Bws	: dimensionless				
	Vwstd/(Vwstd+Vmstd)	0.0079	0.0107	0.0096	0.0094
7. Md	: mol.wt. dry basis				
	.44 CO2+.32 O2+.28(CO+N2)	28.836	28.836	28.836	
8. Ms	: mol.wt. wet basis				
	Md(1-Bws)+18 Bws	28.75	28.72	28.73	
9. Vs	: ft/sec				
	Kp Cp (sqrDP)sqr(Ts/(Ps Ms))	50.10	57.25	49.34	52.23
10. Q	: cfm				
	Vs As(60 sec/min)	70878	80996	69798	73891
11. Qstw	: scfm				
	Q(Ps/Pstd)(Tstd/Ts)	67032	77158	66455	70215
12. Qstd	: dscfm				
	Qstw(1-Bws)	66501	76336	65819	69552
13. I	: percent				
	[(100 Ts)(.002669 Vic+(Vm Pm/Tm))/(60 theta Vs Ps An)	99.07	100.69	98.69	99.49

VOC Loading

14. CVOC	: ppm as C,dry basis				
	((C,VOC)(3))/(1-bws)	18.99	15.07	20.60	18.22
15. E,VOC	: pounds/hr.				
	(CVOC)(3.12e-8)(Qstd)(60)	0.782	0.710	0.838	0.776

HCOH Loading

16. C,HCOH	: ppm				
	(M,HCOH/Vmstd)(.0283)	37.725	28.333	26.793	30.951
17. E,HCOH	: pounds/hr.				
	(M,HCOH/Vmstd)(Qstd)(60)/(453590000)	11.726	10.109	8.243	10.026

5.0 NOMENCLATURE

SYMBOL	UNITS	DESCRIPTION
An	ft ²	Nozzle cross sectional area
As	ft ²	Stack cross sectional area
Bws	dimensionless	Wet gas fraction
CO ₂	percent	Carbon dioxide content by volume
CO	percent	Carbon monoxide content by volume
Cp	dimensionless	Pitot correction factor
C _X	as labeled	Concentration of pollutant X
DGF	dimensionless	Dry gas fraction
Dn	inches	Nozzle diameter
DH (delta H)	in. H ₂ O	Pressure drop across meter orifice
DP (delta P)	in. H ₂ O	Stack gas velocity pressure
E _X	#/hr	Emission rate of pollutant X
E'X	#/MM Btu	Emission rate of pollutant X
F	dscf	Volume of flue gas per MM Btu
I	percent	Nozzle velocity/stack gas velocity
Kp	consistent	Pitot tube constant
M _X	milligrams	Sample weight of pollutant X
Md	### mole	Dry molecular weight of stack gas
Ms	### mole	Wet molecular weight of stack gas
N ₂	percent	Nitrogen content by volume, dry basis
O ₂	percent	Oxygen content by volume, dry basis
Pbar	in. Hg	Barometric pressure
Pg	in. Hg	Stack static pressure
Pm	in. Hg	Total pressure at meter (Pbar+(DH/13.6))
Ps	in. Hg	Total stack pressure (Pbar+(Pg/13.6))
Pstd	in. Hg	Standard barometric pressure = 29.92
Q	acfm	Volumetric flow rate at stack conditions
Qstd	dscfm	Volumetric flow rate at standard conditions, dry basis
Qstdw	scfm	Volumetric flow rate at standard conditions, wet basis
q (theta)	minutes	Sample duration
tm	°F	Meter temperature (Tm denotes °R)
ts	°F	Stack temperature (Ts denotes °R)
Tstd	°R	Standard temperature = 528°R
Vlc	ml	volume of water collected
Vm	ft ³	Volume of dry gas sampled through meter
Vmstd	dscf	Sample volume at standard conditions
Vwstd	scf	Sample volume of water vapor
Y	dimensionless	Meter coefficient
Xsair	percent	Excess air

6.0 CALIBRATIONS Measurement devices used by Environmental Monitoring Laboratories and subject to changes in measurement precision are initially calibrated prior to use. Those instruments for which calibration factors are subject to change or for which calibration checks are required, are calibrated following each field use or as otherwise directed and noted. Calibration procedures for specific equipment are as follows.

Dry Gas Meter:

Dry gas meters are periodically removed from the sampling consoles and cleaned and repaired (new gaskets etc. as required). Following the overhaul of a meter, the measuring precision is checked by the Bell Prover Method and adjusted when necessary to read to within 2% of 100% accuracy. This service is provided by Big Three Meter Company in Jackson, Mississippi. Overhaul service or any six month period is followed by a five point calibration described in APTD-0576 using either a wet test meter or calibrated dry gas meter (used exclusively for calibrations) as a standard reference. Following field use, a gas meter calibration is checked in one of two ways. [1] Three calibration checks at intermediate orifice settings are performed or [2] orifice meter coefficients are used.

If a meter coefficient obtained from pre-test and post-test checks differs by more than 5%, the coefficient (Y) giving the lower sample volume is used in the calculations.

Orifice:

The orifice coefficient is initially determined and is rechecked following a major gas meter repair and calibration.

Nozzles:

Nozzles are checked before each field use with a precision (.001 in.) dial caliper. Three measurements on different axes are made; an average of those three readings is used in calculations. If the tolerance among measurements exceeds 0.004 inches (highest to lowest reading) the nozzle is repaired and recalibrated or discarded.

Pitot Tubes:

Pitot tubes meeting EPA geometry standards are assigned a coefficient of 0.84. Pitot tubes are visually inspected for damage before, during and after use. Those pitot tubes not meeting the geometry standards are assigned a coefficient from the manufacturer's calibration which it retains unless damaged. All pitot tubes used by Environmental Monitoring Laboratories are manufactured by NAPP, Inc.

Temperature Measuring Instruments:

Most temperature measurements are made with a type K thermocouple and an Omega digital thermocouple thermometer which has an initial calibration traceable to NBS. Other measurements are made using bimetallic dial thermometers. The thermocouples and dial thermometers are checked following or during a test series against an ASTM mercury in glass thermometer.

Barometer:

Aneroid field barometers are checked against and adjusted to readings from a mercury barometer or readings obtained from local weather authorities.

Differential Pressure Gauges:

Velocity head (ΔP) and orifice pressure differential (ΔH) measurements are made using water manometers of the appropriate range unless otherwise noted in the test data. Manometers do not require calibration.

Flame Ionization Detector (FID):

VOC measurements were made with a Ratfisch portable flame ionization detector set in a range of 0 to 100 ppm or 0 to 1000 ppm propane. Following a sufficient warm up period the instrument was set to respond to and measure 22.1 ppm and 796 ppm calibration propane. Prior to and following each sample run, the instrument's zero and span were checked and adjusted if necessary using supplies of air and calibration propane.

Non-dispersive Infrared Analyzer (NDIR):

Carbon monoxide measurements are made with a Beckman 864 infrared instrument calibrated in ranges of 0 to 1000 ppm and 0 to 5000 ppm. Following a sufficient warm up period of at least 1 hour and prior to each sample run, the instrument's zero and span are checked and adjusted if necessary using a supply of 100% nitrogen and 850 ppm CO respectively. An intermediate check at 150 ppm CO is also performed. These calibrations and adjustments are repeated at the conclusion of each sampling period.

Chemiluminescent NOx Analyzer:

Nitrogen oxide concentrations measurements are made with a multi-range TECO Model 10-S NOx analyzer. Following a sufficient warm up period and prior to each sample run, the instrument's zero and span are checked and adjusted if necessary using a supply of zero air and 86 ppm protocol 1 nitrogen dioxide. These calibrations and adjustments are repeated at the conclusion of the sampling period.

7.0 APPENDICES

- A. Sampling and Analytical Data
- B. Recorder Traces/Data Log
- C. Calibration Data
- D. Formaldehyde Analysis (ATI)
- E. Armstrong Environmental Report
- F. Louisiana Pacific Production Summaries

7.0 APPENDICES

APPENDIX A.

SAMPLING AND ANALYTICAL DATA

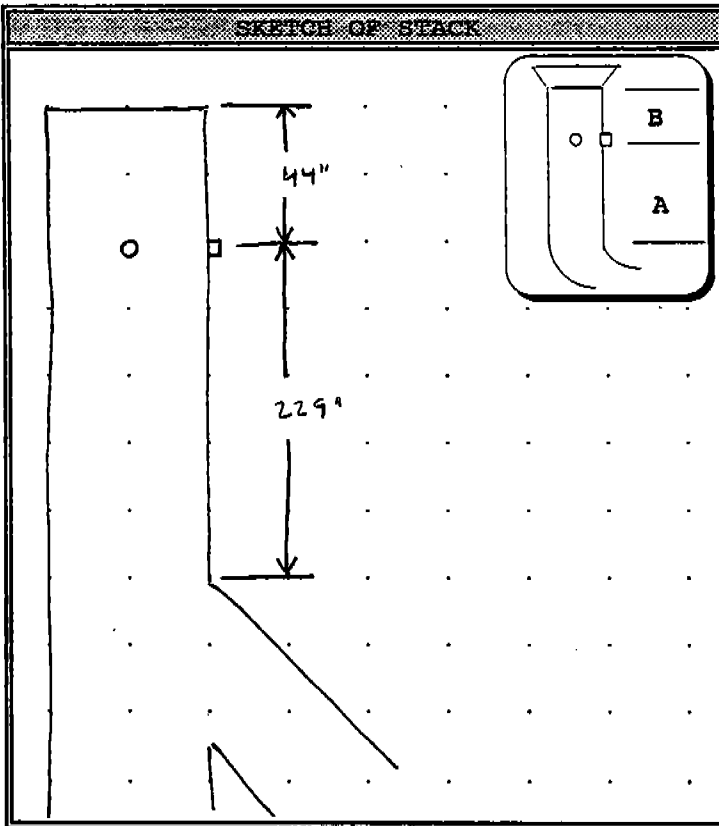
MDF DRYERS

NORTH RTO

PM/CO/NO_x EMISSIONS TEST

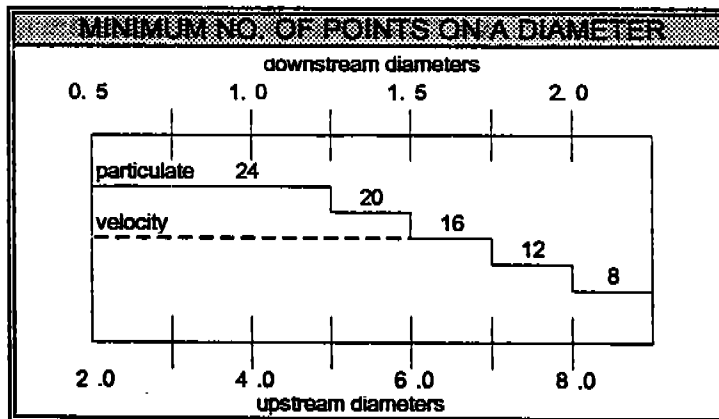
STACK CONFIGURATION AND SAMPLE POINT LAYOUT FOR CIRCULAR STACKS

PLANT: Louisiana Pacific - Urania Date: _____
SOURCE: MDP Paper RTO Outlet - NORTH
TEST FOR: PM Setup
TEST OPERATORS: Russell

[illegible]

Point No.	Inches from wall	velocity head
1	1.8	
2	5.7	
3	10.1	
4	15.1	
5	21.4	
6	30.4	
7	55.1	
8	64.1	
9	70.4	
10	75.4	
11	79.8	
12	83.3	

STACK DIAMETER:	<u>85.5</u>
Distance from ports to disturbance:	
A. to upstream disturbance	<u>239'</u>
B. to downstream disturbance	<u>44'</u>
Upstream diameters:	<u>2.68</u>
Downstream diameters:	<u>0.51</u>
Minimum No. sample points required:	<u>24</u>
No. sample points selected:	<u>12 x 2</u>
Port Length:	<u>4.0"</u>
Port Type:	<u>4" pipe nipple</u>
Port Access:	<u>platform / manhole</u>



Pitot ID :	Pitot Cp:	Stack Temp:
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Remarks:

Plant Louisiana Pacific - Meria Louisiana MDE Plant
 Sampling Location Dayton North RTO
 Test For PM/NOx/CO
 Test Operators Russell/McKnight

RUN No. 1
 Date 1-18-94
 Time start 1115 end 1218

Meter Box	<u>Anderson</u>	No. Sample Pts.	<u>12x2</u>	Gas Analysis	<u>int. BAC</u>	Remarks: <u>Nozzle Cd:</u> <u>10 .242</u> <u>11 .242</u> <u>12 .243</u>
Sample Box	<u>No. 3</u>	Minutes/Pt.	<u>2.5</u>	CO ₂	<u>Wet = 1.0</u>	
Probe/Pitot	<u>0.5655</u>			O ₂	<u>Sewerex = 19.8</u>	
Pitot Cp	<u>.84</u>	NOMOGRAPH		CO	<u>TECO 48 = 5.1</u>	
Nozzle Dia.	<u>.242</u>	ΔH@	<u>1.80</u>	Time		
Filter No.		Meter Temp.	<u>100</u>	Condensate:		
		% H ₂ O	<u>15</u>	tare	<u>200</u> fin <u>241</u>	
Amb. Temp. °F	<u>29</u>	C-Factor	<u>.85</u>	Silica gel:		
Bar. Press. "Hg	<u>30.25</u>	Stack Temp.	<u>230</u>	tare	<u>fin 2.0 +</u>	
Static Press. "H ₂ O	<u>-.36</u>	Ref. ΔP	<u>.75</u>			

Port Point	El. Time, Min.	DGM Reading, Ft. ³	Velocity Head Δ P, in. H ₂ O	Orifice Δ H in. H ₂ O	Stack Temp. °F	Meter Temp. °F		Oven Temp. °F	Imp. Temp. °F	Vac in. Hg
						In	Out			
1	000	496.372	0.66	1.60	218	72	72	244	35	2
2	230	498.0	0.62	1.50	217	75	72	249	33	2
3	500	499.9	0.66	1.60	226	81	72	243	33	2
4	730	502.0	0.52	1.25	214	88	74	250	33	2
5	1000	503.5	0.52	1.25	221	89	75	251	33	2
6	1230	505.0	0.39	0.95	217	95	76	250	33	2
7	1500	506.5	0.21	0.75	220	95	76	250	33	2
8	1730	507.7	0.37	0.90	219	97	80	251	34	2
9	2000	509.2	0.42	1.00	216	100	82	248	35	2
10	2230	510.7	0.38	0.92	210	103	85	249	35	2
11	2500	512.0	0.40	0.96	206	104	87	247	36	2
12	2730	513.4	0.35	0.85	210	106	89	251	35	2
1	3000	514.822	0.46	1.10	223	116	85	250	35	2
2	230	516.3	0.42	1.00	201	105	91	252	35	2
3	500	518.0	0.37	0.90	203	108	92	256	35	2
4	730	519.2	0.36	0.86	211	108	93	249	35	2
5	1000	520.6	0.35	0.85	218	110	94	260	35	2
6	1230	522.0	0.35	0.85	207	112	96	250	35	2
7	1500	523.2	0.39	0.95	226	113	97	250	35	2
8	1730	524.7	0.46	1.10	211	114	99	248	35	2
9	2000	525.9	0.32	0.77	221	116	101	250	35	2
10	2230	527.3	0.42	1.00	206	118	102	251	35	2
11	2500	528.6	0.48	1.15	214	122	103	250	35	2
12	2730	530.2	0.27	0.90	210	122	106	250	35	2
end	60	531.233								
Leak Check: .032			→ .037		= .067		4" C 11" Hg			
pitot tube 3.6										
pitot tube 3.2										
35.361		.6531		1.0100		214.79		99.85		

Plant Laudonia PacificSampling Location Danville RTO North DitchTest For PM/CO/NOxTest Operators Russell McKnightRUN No. 2Date 1-18-94Time start 1500 end 1602

Meter Box Anderson
 Sample Box No. 3
 Probe/Pitot 8' SS
 Pitot Cp .84
 Nozzle Dia. .305
 Filter No. _____

No. Sample Pts. 12 x 2
 Minutes/Pt. 2.5

NOMOGRAPH

$\Delta H @$ 1.80
 Meter Temp. 100
 % H₂O 10
 C-Factor .95
 Stack Temp. 230
 Ref. ΔP .28

Gas Analysis int. mg
 CO₂ 0.9
 O₂ Sevenson = 19.8
 CO 3.7 ppm
 Time _____

Condensate:

tare 200 fin 275

Silica gel:

tare _____ fin +3

Remarks:

A 20.7
D 30.5 } 30.5
O 30.6

Port Point	El. Time, Min.	DGM Reading, Ft.	Velocity Head ΔP , in. H ₂ O	Orifice ΔH in. H ₂ O	Stack Temp. °F	Meter Temp., °F In Out	Oven Temp. °F	Imp. Temp. °F	Vac in. Hg
1	000	532.180	0.54	3.55	218	77 74	242	37	3
2	230	534.4	0.52	3.40	225	87 74	242	37	2
3	500	536.9	0.45	2.95	215	98 75	231	37	2
4	730	539.6	0.39	2.50	223	105 77	230	37	2
5	1000	541.8	0.37	2.40	216	110 79	243	38	2
6	1230	544.0	0.34	2.20	227	114 81	237	37	2
7	1500	546.2	0.39	2.55	205	116 83	241	37	2
8	1730	548.1	0.44	2.85	227	120 85	235	37	2
9	2000	550.4	0.50	2.30	214	123 87	235	37	2
10	2230	552.5	0.50	3.30	213	126 89	240	37	2
11	2500	554.7	0.53	3.45	215	128 92	251	38	2
12	2730	557.7	0.48	3.20	206	130 95	244	37	2
14	3000	560.003	0.72	4.70	212	117 97	253	38	2
15	230	562.9	0.74	4.80	229	127 98	246	38	2
16	500	566.2	0.64	4.20	213	131 99	251	38	2
17	730	568.8	0.47	3.20	223	132 100	250	38	2
18	1000	571.3	0.48	3.20	212	133 102	250	38	2
19	1230	573.8	0.40	2.60	231	134 103	250	38	2
20	1500	576.3	0.31	2.00	212	134 104	251	38	2
21	1730	579.0	0.30	2.00	225	133 105	248	38	2
22	2000	580.6	0.32	2.05	214	132 105	244	38	2
23	2230	582.7	0.30	1.95	217	132 106	237	37	2
24	2500	584.8	0.31	2.00	208	133 106	236	36	2
25	2730	586.8	0.32	2.05	206	133 107	237	36	2
26	end 60	588.631							

Leak check: .019 → .062 : .013 ok
 pitot + c 4.4
 pitot - c 3.9

56.451

66.36

2.8917

216.83

106.83

Plant Louisiana Pacific
 Sampling Location MDF RIO North Outlet
 Test For PM/CO/NO_x
 Test Operators Russell / McKnight
 RUN No. 3
 Date 1-18-94
 Time start 1657 and 1802

Meter Box <u>Anderson</u>	No. Sample Pts. <u>512 x 2</u>	Gas Analysis <u>2Ag</u>	Remarks:
Sample Box <u>A-3</u>	Minutes/Pt. <u>2-5</u>	CO ₂ <u>19.8</u> <u>rust</u>	
Probe/Pitot <u>8' 55</u>	NOMOGRAPH	O ₂ <u>20.9</u> <u>5 hex</u>	
Pitot Cp <u>84</u>	ΔH@ <u>1.8</u>	CO _____	
Nozzle Dia. <u>.305</u>	Meter Temp. _____	Time _____	
Filter No. _____	% H ₂ O _____	Condensate:	
Amb. Temp. °F <u>30</u>	C-Factor _____	tare <u>200</u> fin <u>273</u>	
Bar. Press. "Hg <u>29.25</u>	Stack Temp. _____	Silica gel:	
Static Press. "H ₂ O <u>-.3</u>	Ref. ΔP <u>2.8</u>	tare _____ fin <u>7</u>	

Port Point	El. Time, Min.	DGM Reading, Ft. ³	Velocity Head ΔP, in. H ₂ O	Orifice ΔH in. H ₂ O	Stack Temp. °F	Meter Temp., °F In	Meter Temp., °F Out	Oven Temp. °F	Imp. Temp. °F	Vac in. Hg
1	00	589.757	0.79	5.40	219	89	83	235	35	4
2	230	592.4	0.76	5.00	212	93	83	235	35	7
3	500	595.3	0.67	4.40	215	101	83	247	34	4
4	730	598.1	0.57	3.70	209	108	85	251	35	7
5	1000	600.8	0.52	3.40	213	112	86	255	35	7
6	1230	603.6	0.39	2.55	208	116	86	255	35	7
7	1500	606.0	0.30	2.00	203	116	89	250	35	7
8	1730	608.3	0.29	1.90	208	117	92	250	35	7
9	2000	609.7	0.28	1.85	206	117	94	250	35	7
10	2230	611.5	0.30	2.00	210	118	95	235	35	7
11	2500	613.5	0.32	2.10	206	121	97	235	35	7
12	2730	616.2	0.32	2.10	207	123	99	236	35	7
1	3000	617.628	0.48	3.20	203	104	97	240	35	3
2	230	620.0	0.49	3.25	220	112	99	245	35	3
3	500	622.5	0.45	2.95	206	121	99	230	37	3
4	730	624.7	0.42	2.80	217	125	100	243	35	3
5	1000	627.3	0.38	2.45	212	127	101	238	35	3
6	1230	629.7	0.24	2.20	213	130	103	238	35	3
7	1500	631.6	0.40	2.60	205	129	104	240	35	3
8	1730	633.9	0.42	2.80	210	131	106	251	25	3
9	2000	636.6	0.46	3.00	205	134	107	252	35	5
10	2230	638.7	0.48	3.20	207	136	109	253	26	3
11	2500	640.8	0.50	3.30	213	138	110	254	36	3
12	2730	643.5	0.46	3.00	201	139	112	252	35	3
and	60	645.883								
lack check: .071 → .045 = .014 <i>ape</i> 11" <i>Hy</i> pitot + ve 5.0 pitot - ve 4.0 56.426 .6634 2.9646 209.50 107.90										

SAMPLES:

L.P. - Urania MOF / Dryers RTO North

DATE TAKEN:

1-18-94

DATE ANALYZED:

1-23-94

DELIVERED BY:

DCR

RECEIVED BY:

DCR

ANALYZED BY:

DCR

(Attach chain of custody if additional exchanges occur)

FILTERS:

RUN NO.	1	2	3	
FILTER NO.	532	533	535	
FILTER TARE, gms.	.5613	.5629	.5614	
	.5707	.6058	.5005	
	.5706	.6058	.5803	
FINAL WEIGHT, gms.	.5706	.6058	.5803	
NET GAIN, gms.	.0093	.0877	.0189	

PROBE WASH:

RUN NO.	1	2	3	
CONTAINER I.D.	N-RTO R1	N-RTO R2	N-RTO R3	
VOLUME INTACT?	✓	✓	✓	
VOLUME, ml	150	140	140	
TARE WEIGHT, gms.	(80) 107.9648	(81) 104.6001	(85) 109.1496	114.1933
	107.9772	104.6140	109.1639	114.1932
	107.9773	104.6135	109.1635	114.1932
FINAL WEIGHT, gms.	107.9773	104.6135	109.1635	114.1933
NET GAIN, gms.	.0125	.0134	.0139	-0-
LESS BLANK, gms.	-0-	-0-	-0-	

PARTICULATE SAMPLE WEIGHT:

RUN NO.	1	2	3	
filter + probe, mg.	21.8	51.1	32.8	

PARTICULATE CATCH ANALYSIS

(Back Half Methylene Chloride Extraction)

SAMPLES:

L.P. - Dryers RTO North

DATE TAKEN:

1-18-94

DATE ANALYZED:

1-26-94

DELIVERED BY:

DEB

RECEIVED BY:

DEB

ANALYZED BY:

DEB

(Attach chain of custody if additional exchanges occur)

AQUEOUS FRACTION:

RUN NO.	1	2	3	
CONTAINER ID.	NRTOR1 BAK	NRTOR2 BAK	NRTOR3 BAK	
VOLUME INTACT?	✓	✓	✓	
VOLUME, ml	300	300	300	
TARE WEIGHT, gms.	(9) 114.8140	(61) 113.9826	(67) 111.4659	
	114.8171	113.9845	111.4685	
	114.8168	113.9847	111.4680	
FINAL WEIGHT, gms.	114.8163	113.9847	111.4680	
NET GAIN, gms.	.0028	.0021	.0021	
LESS BLANK, gms.				

ORGANIC FRACTION

3 25ml extractions w/ methylene chloride

RUN NO.				
CONTAINER ID.	Same as above			
VOLUME INTACT?	✓	✓	✓	
VOLUME, ml				
TARE WEIGHT, gms.	(2) 104.7502	(84) 105.3498	(87) 107.2274	
	104.7507	105.3513	107.2293	
	104.7503	105.3513	107.2290	
FINAL WEIGHT, gms.	104.7503	105.3513	107.2290	
NET GAIN, gms.	.0001	.0015	.0016	
LESS BLANK, gms.				

PARTICULATE SAMPLE WEIGHT:

RUN NO.	1	2	3	
Aqueous fraction, mg	2.8	2.1	2.1	
Organic fraction, mg	0.1	1.5	1.6	

Ag
NR5

MDF DRYERS

NORTH RTO

VOC/HCOH EMISSIONS TEST

Plant Louisiana Pacific - Urania MDF
 Sampling Location North MDF ATO Outlet
 Test For HCHOH / VOC
 Test Operators Russell McKnight

RUN No. 1
 Date 1-19-94
 Time start 1106 end 1506

Meter Box Anderson
 Sample Box No. 3
 Probe/Pitot 8' Teflon
 Pitot Cp 84
 Nozzle Dia. .277 GAS
 Filter No.

No. Sample Pts. 1202
 Minutes/Pt. 2.5

NOMOGRAPH
 $\Delta H @$ 1.80
 Meter Temp. 100
 % H₂O 10
 C-Factor .95
 Stack Temp. 220
 Ref. ΔP .39

Gas Analysis int. GAS
 CO₂ 1.0
 O₂ 19.8
 CO
 Time

Condensate:
 tare Ramcke fin
 Silica gel:
 tare Ramcke fin

Remarks:
0.277
0.277 } .277
0.277
dry down 1136
up 1434
 1) DNPH 576.5 625.5
 2) DNPH 577.0 588.5
 3) MT 477.5 478.5
 4) SGH 780.5 791.0

Port Point	El. Time, Min.	DGM Reading, Ft. ²	Velocity Head ΔP , in. H ₂ O	Orifice ΔH in. H ₂ O	Stack Temp. °F	Meter Temp., °F In	Meter Temp., °F Out	Oven Temp. °F	Imp. Temp. °F	Vac in. Hg
1	000	646.523	0.50	2.40	211	67	67	N/A	38	2
2	230	648.2	0.51	2.40	235	73	66		38	2
3	500	650.2	0.47	2.25	213	78	66		38	2
4	730	651.6	0.43	2.10	219	82	67		38	2
5	1000	654.4	0.41	1.95	212	89	69		38	3
6	1230	656.4	0.38	1.80	228	94	69		39	3
7	1500	658.0	0.37	1.75	212	96	72		39	3
8	1730	659.9	0.45	2.20	226	100	74		39	2
9	2000	661.8	0.47	2.20	237	102	75		40	2
10	2230	663.8	0.49	2.25	216	107	74		40	2
11	2500	665.7	0.50	2.40	233	109	81		40	2
12	2730	668.0	0.46	2.20	219	113	84		40	2
1136										
14381	30/00	669.672	0.71	3.40	226	70	70		40	2
2	230	672.0	0.72	3.40	205	73	69		40	2
3	500	674.7	0.68	3.00	224	82	70		41	2
4	730	677.0	0.56	2.60	204	92	72		42	2
5	1000	679.1	0.50	2.40	216	97	73		43	2
6	1230	681.7	0.43	2.05	210	100	75		43	2
7	1500	683.5	0.30	1.45	220	104	78		43	2
8	1730	685.2	0.28	1.35	211	104	80		44	2
9	2000	686.7	0.30	1.45	227	105	82		48	2
10	2230	688.2	0.30	1.45	214	106	84		49	2
11	2500	689.9	0.28	1.35	223	108	86		51	2
12	2730	691.8	0.30	1.45	214	110	89		51	2
end	60	693.163								

lack duct : .055 - .062 = .007 at e 8" K
 pitot + e 4.0
 pitot - e 3.3
 46.640
 .6634
 2.1396
 218.96
 84.63

Plant Louisiana Pacific - Urethane MOF
 Sampling Location MOF North RTO
 Test For VOC/HCOM
 Test Operators Romero/McKnight

RUN No. 2
 Date 1-19-94
 Time start 1627 end 1729

Meter Box Anderson
 Sample Box 10.3
 Probe/Pitot 8" Teflon
 Pitot Cp 84
 Nozzle Dia. 2.77
 Filter No.

No. Sample Pts. 12 x 2
 Minutes/Pt. 2.5

NOMOGRAPH
 $\Delta H @$ 1.8
 Meter Temp.
 % H₂O
 C-Factor
 Stack Temp.
 Ref. ΔP .35

Gas Analysis int. BAG
 CO₂ 0.9
 O₂ 19.8
 CO
 Time

Condensate:
 tare Romero fin
 Silica gel:
 tare fin

Remarks: tare Final
1 DNPH 579.5 650.0
2 DNPH 575.0 580.0
3 mt 477.5 478.5
45. Gel 725.5 747.5

Amb. Temp. °F 40
 Bar. Press. "Hg 30.28
 Static Press. "H₂O -.22

Port Point	El. Time, Min.	DGM Reading, Ft. ³	Velocity Head ΔP , in. H ₂ O	Orifice ΔH in. H ₂ O	Stack Temp. °F	Meter Temp., °F In Out	Oven Temp. °F	Imp. Temp. °F	Vac in. Hg
1	200	694.673	0.50	2.40	228	76 76	N/A	40	2
2	230	696.6	0.52	2.45	224	81 77		42	2
3	500	699.2	0.48	2.30	226	87 77		44	2
4	730	701.1	0.40	1.80	234	94 78		44	2
5	1000	702.9	0.33	1.55	231	97 79		44	2
6	1230	704.8	0.32	1.50	225	101 81		44	2
7	1500	706.4	0.40	1.90	227	103 83		44	2
8	1730	708.2	0.44	2.10	222	105 84		45	2
9	2000	709.9	0.42	2.00	236	110 86		45	2
10	2230	712.4	0.46	2.20	224	115 90		46	2
11	2500	714.0	0.44	2.10	232	117 91		46	2
12	2730	716.1	0.44	2.10	217	120 94		46	2
1	30/60	718.235	0.70	3.35	222	113 96		47	3
2	230	720.7	0.71	3.40	229	121 98		49	3
3	500	723.2	0.68	3.30	234	127 100		51	4
4	730	725.8	0.59	2.80	232	131 102		50	4
5	1000	728.2	0.46	2.15	222	131 104		50	4
6	1230	730.2	0.40	1.80	226	130 105		50	4
7	1500	732.1	0.25	1.70	229	128 106		51	4
8	1730	734.1	0.30	1.40	224	127 107		51	4
9	2000	735.6	0.29	1.40	235	125 107		52	4
10	2230	737.6	0.30	1.40	225	124 108		50	4
11	2500	739.1	0.30	1.45	232	124 108		50	4
12	2730	740.9	0.30	1.45	214	124 108		50	4
and	60	742.735							
leak back: 1047 → .052 pitot +ve 3.9 pitot -ve 3.5 48.062 .6561 2.0833 227.08 103.25									

Plant Louisiana Pacific - Ureia M.D.FSampling Location M.D.F North RTDTest For VOC/HCOHTest Operators Russell/McKnightRUN No. 3Date 1-19-94Time start 1214 and 1915Meter Box AndersonSample Box No. 3Probe/Pitot 8' teflonPitot Cp .84Nozzle Dia. .277 inFilter No. Amb. Temp. °F 38Bar. Press. "Hg 30.28Static Press. "H₂O -.36No. Sample Pts. 12 x 2Minutes/Pt. 2.5

NOMOGRAPH

ΔH@ 1.8Meter Temp. % H₂O C-Factor Stack Temp. Ref. ΔP .39Gas Analysis BAG-INCO₂ 0.9O₂ 19.8CO Time

Condensate:

tare 200 fin

Silica gel:

tare fin

Remarks:

1) DNPH 575.0 / 652.0

2) DNPH 576.0 / 597.5

3) MT 477.5 / 478.5

4) S.G. 747.5 / 757.0

Port Point	El. Time, Min.	DGM Reading, Ft. ³	Velocity Head ΔP, in. H ₂ O	Orifice ΔH in. H ₂ O	Stack Temp. °F	Meter Temp., °F In	Meter Temp., °F Out	Oven Temp. °F	Imp. Temp. °F	Vac. in. Hg
1	0000	743.111	0.74	3.65	222	85	85	N/A	38	4
2	230	745.6	0.73	3.50	233	100	86		40	4
3	500	748.1	0.65	3.10	226	108	86		42	4
4	730	750.6	0.60	2.85	226	114	87		44	4
5	1000	753.2	0.47	2.25	219	117	88		45	4
6	1230	755.4	0.44	2.15	226	120	89		45	4
7	1500	757.2	0.32	1.50	239	119	90		42	3
8	1730	759.0	0.30	1.40	226	119	91		43	3
9	2000	764.5	0.30	1.40	228	119	91		44	3
10	2230	762.2	0.30	1.40	219	121	92		48	3
11	2500	763.7	0.32	1.55	235	124	95		44	3
12	2730	765.5	0.30	1.40	222	126	96		44	3
1	3000	767.177	0.49	2.35	225	114	98		44	3
2	230	769.3	0.50	2.40	233	124	99		44	3
3	500	771.4	0.44	2.15	221	128	100		44	3
4	730	773.5	0.37	1.75	236	129	101		44	3
5	1000	775.6	0.35	1.65	224	130	102		44	3
6	1230	777.4	0.30	1.45	233	129	103		44	3
7	1500	779.1	0.38	1.80	233	129	103		42	3
8	1730	780.8	0.39	1.85	231	130	105		42	3
9	2000	782.5	0.46	2.20	219	132	106		41	3
10	2230	785.1	0.43	2.10	232	134	106		41	3
11	2500	786.6	0.46	2.20	216	135	107		41	4
12	2730	788.6	0.50	2.40	219	136	108		40	4
1	3000	790.816								

Lock the k: .012 → .014 = .002 gpc 10' Hg

pit + 4 = 7.6

pit - 4 = 3.5

47.105

.6560

2.1021

226.79

108.23

MDF DRYERS

RTO INLET

PM/CO/NO_x INLET LOADING TEST

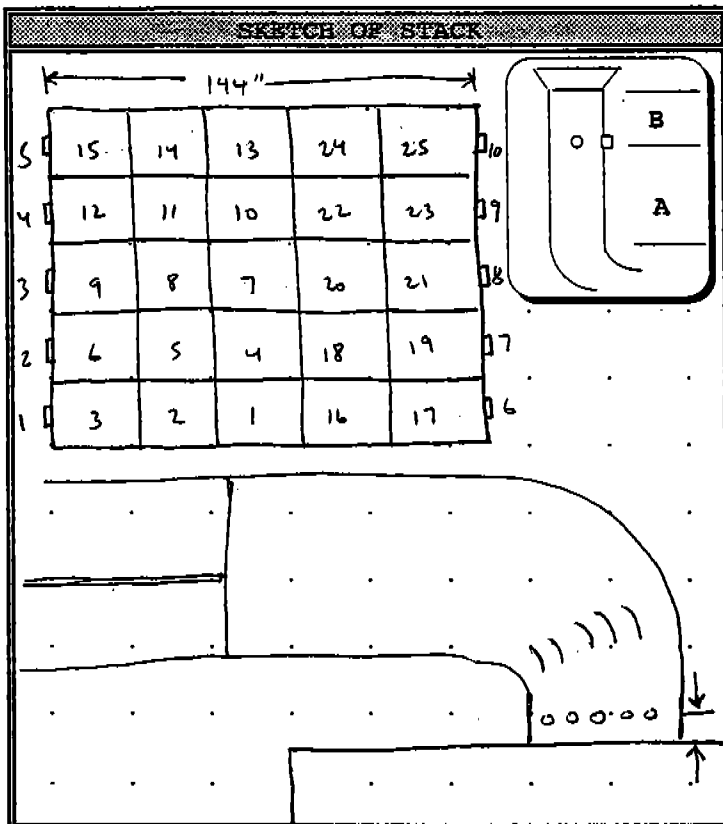
STACK CONFIGURATION AND SAMPLE POINT LAYOUT FOR CIRCULAR STACKS

PLANT: Louisiana Pacific - Urania Date: _____

SOURCE: Dryers RTD Balot

TEST FOR: PM Setup

TEST OPERATORS: Russell



PERCENT OF DIAMETER

point no.	points on a diameter							
	2	4	6	8	10	12	14	16
1	14.6	6.7	4.4	3.2	2.6	2.1	1.8	1.6
2	85.4	25.0	14.6	10.5	8.2	6.7	5.7	4.9
3		75.0	29.6	19.4	14.6	11.8	9.9	8.5
4		93.3	70.4	32.3	22.6	17.7	14.6	12.5
5			85.4	67.7	34.2	25.0	20.1	16.9
6			95.6	80.6	65.8	35.6	26.9	22.0
7				89.5	77.4	64.4	36.6	28.3
8				96.8	85.4	75.0	63.4	37.5
9					91.8	82.3	73.1	62.5
10					97.4	88.2	79.9	71.7
11						93.3	85.4	78.0
12						97.9	90.1	83.1
13							94.3	87.5
14							98.2	91.5
15								95.1
16								98.4

STACK DIAMETER: 144" x 94"

Distance from ports to disturbance:

A. to upstream disturbance _____

B. to downstream disturbance _____

Upstream diameters: _____

Downstream diameters: _____

Minimum No. sample points required: _____

No. sample points selected: _____

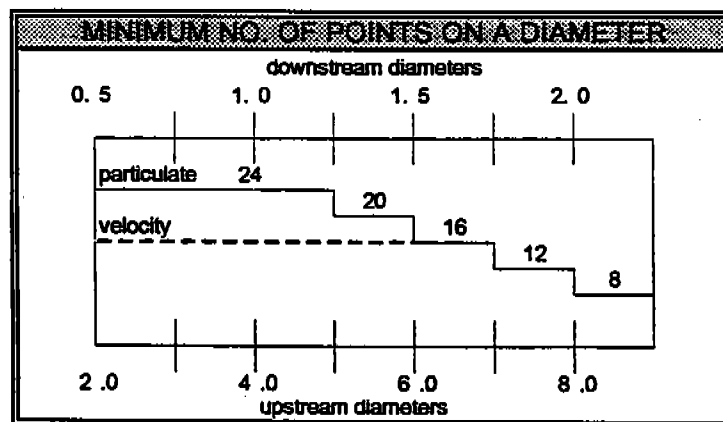
Port Length: _____

Port Type: 4" pipe nipple

Port Access: Platform Boards

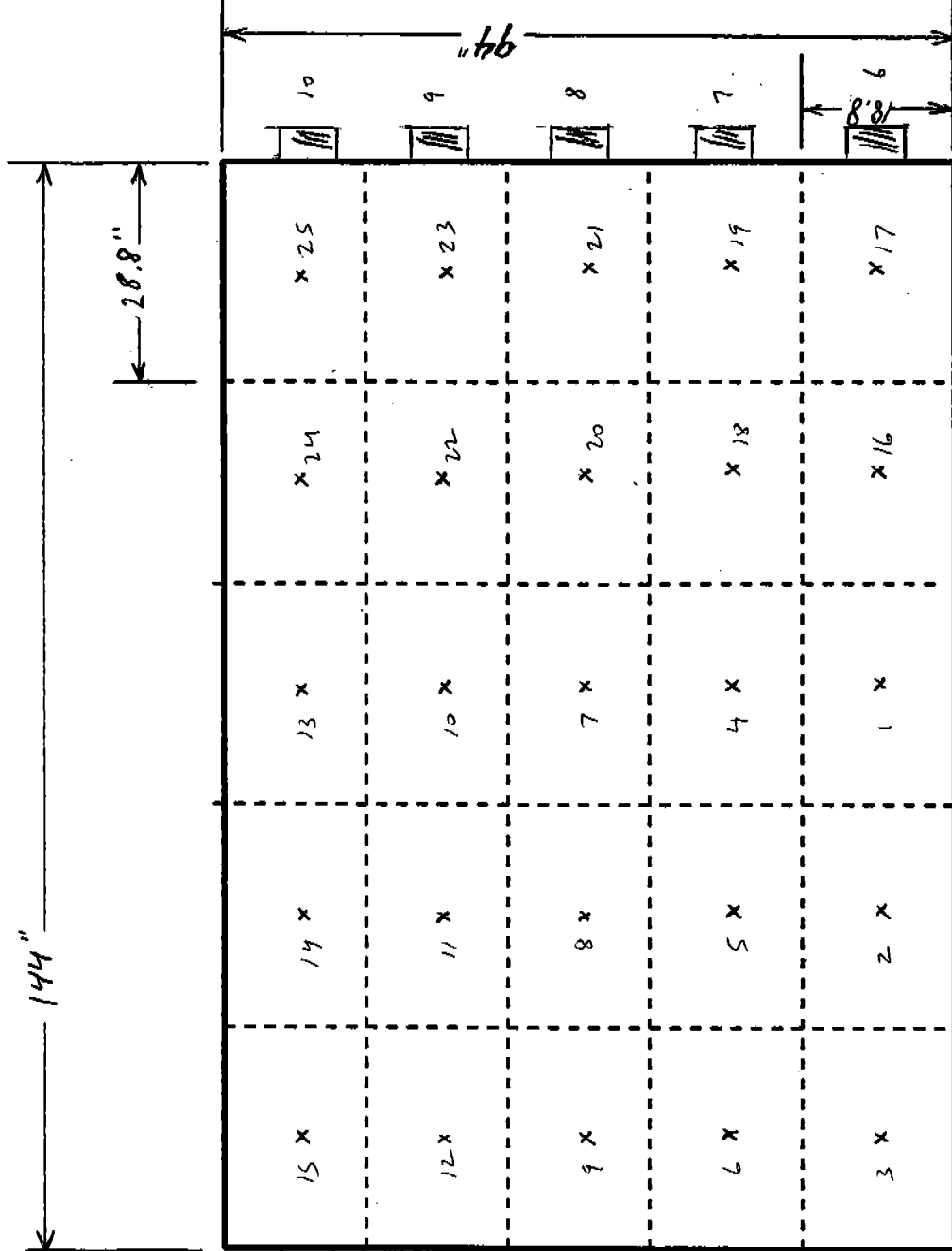
velocity head

Point No.	Inches from wall	DP	DP	DP	DP	DP	DP	DP
1	72.0	.82	.06	L	14	.05	0	
2	43.2	.83	.10	L	15	.05	0	
3	14.4	1.30	.12	L	16	1.35	5R	
4		.57	.5	L	17	1.40	3R	
5		.45	.4	L	18	.70	0	
6		.38	0		19	.67	0	
7		.30	0		20	.32	0	
8		.23	0		21	.32	0	
9		.28	0		22	.14	0	
10		.05	0		23	.18	0	
11		.18	0		24	.07	0	
12		.18	0		25	.05	0	
13		.05	0					



Pitot ID: _____ Pitot Cp: _____ Stack Temp: _____

Remarks:



4" Pipe nipple
(10) on 18.8" centers

3 2 1

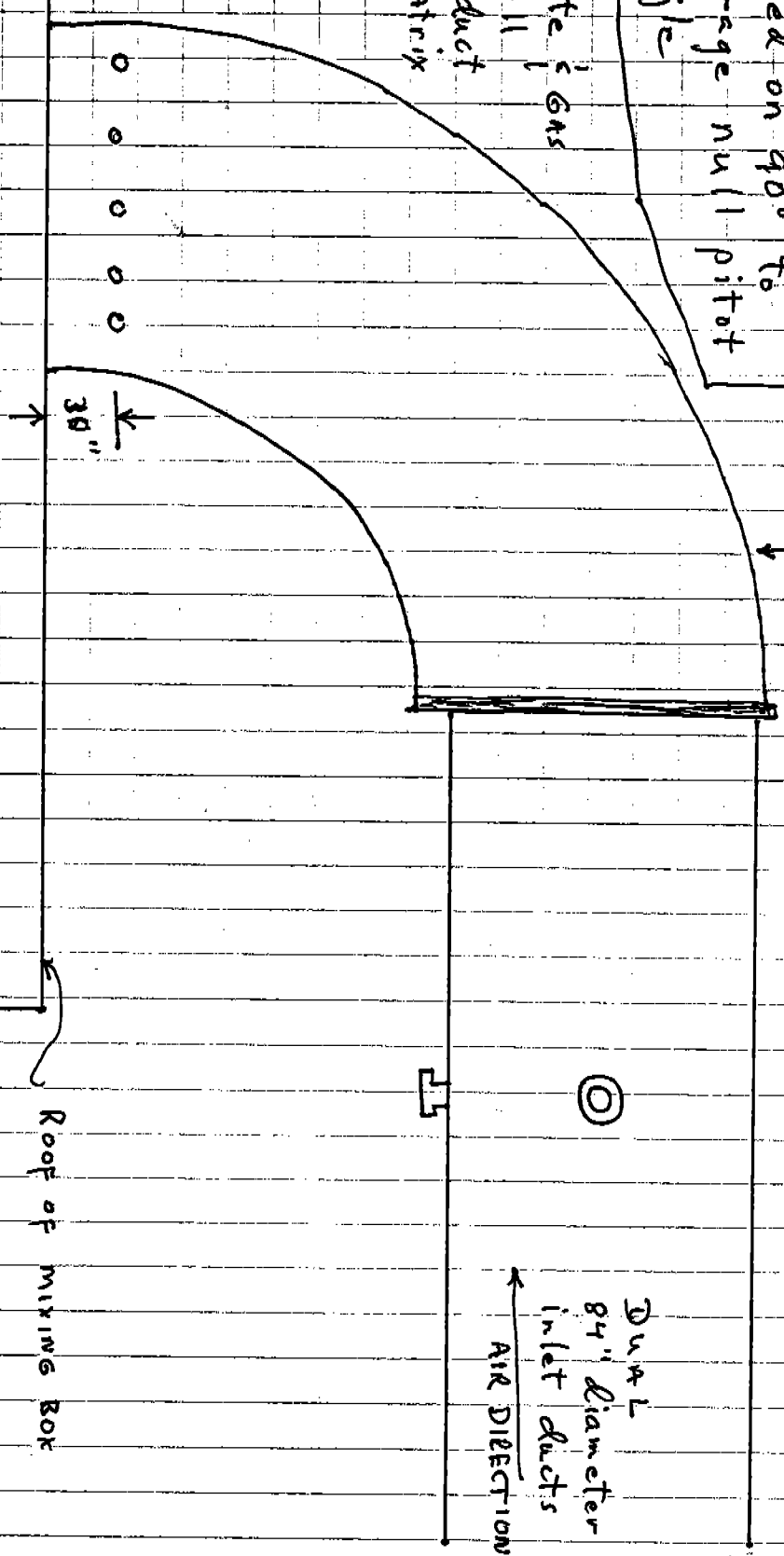
L.P. Urania, Louisiana
RTD inlet configuration
 + proposed sampling site

Sample probe will be directed into flow based on 90° to Average null pitot angle

Mixing Box inlet is 144" x 94" rectangular duct with 90° bend on 144" radius

Particulate & Gas Probes will traverse duct on 5x5 matrix

Proposed sample port location



Flow direction
 144" radius

Plant Louisiana Pacific - Urethane, LouisianaSampling Location Dryers RTO InletTest For pm / CO₂ / COTest Operators RussellRUN No. 1Date 1/16/94Time start 1114 end 1223Meter Box RAC591349Sample Box 4Probe/Pitot 6" i.c.Pitot Cp .84Nozzle Dia. .272Filter No. Amb. Temp. °F 29Bar. Press. "Hg 30.25Static Press. "H₂O -1.6No. Sample Pts. 25(5x5)Minutes/Pt. 2.5

NOMOGRAPH

ΔH@ 1.25Meter Temp. 100% H₂O 15C-Factor 100.91Stack Temp. 120Ref. ΔP .36Gas Analysis OKCO₂ 1.0O₂ 19.8CO Time

Condensate:

tare 200 fin 30 252

Silica gel:

tare fin 46Remarks: 11.22/120.2720.272 0.2720.272dryer down 13.18

Port Point	El. Time, Min.	DGM Reading, Ft.	Velocity Head ΔP, in. H ₂ O	Orifice ΔH, in. H ₂ O	Stack Temp. °F	Meter Temp., °F In	Meter Temp., °F Out	Oven Temp. °F	Imp. Temp. °F	Vac in. Hg
1 1	000	649.776	0.80	4.20	128	77	77	244	35	2
2 2	230	652.4	0.83	4.30	125	81	76	251	34	3
3 3	500	655.6	0.20	6.40	124	84	78	252	34	7
2 4	730	658.913	0.56	2.90	119	98	83	253	29	7
5 5	1000	662.1	0.38	1.95	121	101	86	250	32	7
6 6	1230	663.8	0.52	2.70	121	105	83	243	34	3
3 7	1500	660.010	0.27	1.90	118	107	82	250	24	2
8 8	1730	667.3	0.23	1.20	118	110	84	250	35	2
9 9	2000	668.9	0.27	1.90	117	109	84	250	32	2
4 10	2230	670.332	0.10	0.51	118	108	85	243	22	2
11 11	2500	671.3	0.08	0.41	115	108	86	252	37	2
12 12	2730	672.3	0.13	0.66	111	110	87	246	35	2
5 13	3000	673.302	0.06	0.31	111	109	89	249	25	2
14 14	3230	674.2	0.06	0.31	112	112	94	241	35	2
15 15	3500	675.2	0.06	0.31	102	112	91	249	35	2
6 16	3730	675.908	0.20	6.30	118	111	95	242	25	5
17 17	4000	679.2	1.20	6.30	119	113	95	248	35	5
7 18	4230	682.424	0.65	3.40	120	122	96	252	35	5
19 19	4500	684.9	0.56	2.90	121	127	98	250	35	5
8 20	4730	687.361	0.22	1.65	119	127	99	251	26	2
21 21	5000	689.1	0.30	1.55	122	129	100	250	36	3
9 22	5230	690.681	0.18	0.96	118	124	100	250	26	2
23 23	5500	692.4	0.20	1.05	115	128	102	249	36	3
10 24	5730	694.000	0.08	0.42	113	123	102	250	26	3
25 25	6000	694.9	0.10	0.51	113	125	98	250	26	3
and 26	6230	695.828								

Leak check: .033 → .040 = .007 cf e 11 "H₂

pilot + 4.8

pilot - 4.5

46.052

.5553

2.1603

117.52

100.20

Plant Louisiana Pacific - Urdonia, Louisiana
 Sampling Location Dryden OSE RTO Inlet
 Test For PAH/CO/NOx
 Test Operators Rhonda Moore

RUN No. 2
 Date 1-18-94
 Time start 1759 end 1607

Meter Box RAK 591349
 Sample Box N₂
 Probe/Pitot 6.55
 Pitot Cp .84
 Nozzle Dia. .272
 Filter No.

No. Sample Pts. 5 x 5
 Minutes/Pt. 2.5

NOMOGRAPH

$\Delta H @$ 1.85
 Meter Temp. 100
 % H₂O 10
 C-Factor .98
 Stack Temp. 125
 Ref. ΔP .35

Gas Analysis Dry
 CO₂ 1.0
 O₂ 19.0
 CO
 Time

Condensate:
 tare 200 fin 259
 Silica gel:
 tare fin +11

Remarks:

Port Point	El. Time, Min.	DGM Reading, Ft. ³	Velocity Head ΔP , in. H ₂ O	Orifice ΔH in. H ₂ O	Stack Temp. °F	Meter Temp., °F In Out	Oven Temp. °F	Imp. Temp. °F	Vac. in. Hg
1 1	000	696.164	0.71	2.90	121	83 82	234	38	3
2 2	230	699.0	0.90	4.90	121	85 84	245	36	3
3 3	500	701.7	1.25	6.80	120	89 82	245	36	3
2 4	730	705.595	0.41	2.20	119	102 83	245	36	2
5 5	1000	707.9	0.39	2.10	123	102 85	248	28	3
6 6	1230	709.9	0.58	3.20	121	109 85	248	34	3
3 7	1500	712.500	0.22	1.20	121	104 86	250	38	2
8 8	1730	714.5	0.22	1.20	120	106 87	249	38	3
9 9	2000	716.6	0.20	1.60	122	117 86	250	30	3
4 10	2230	718.415	0.13	0.70	119	113 87	251	38	3
11 11	2500	719.4	0.17	0.91	120	113 90	252	36	3
12 12	2730	721.0	0.16	0.85	115	114 92	249	37	2
5 13	3000	722.292	0.07	0.37	109	113 91	243	37	2
14 14	3230	723.3	0.07	0.27	119	114 92	248	27	2
15 15	3500	724.2	0.08	0.42	115	114 93	254	38	2
6 16	3730	725.052	1.20	6.50	120	114 93	250	34	4
17 17	4000	728.8	1.20	6.50	122	120 96	250	34	4
7 18	4230	732.000	0.77	4.20	721	125 94	245	29	4
19 19	4500	736.3	0.61	3.40	120	136 102	244	29	4
8 20	4730	737.5	0.33	1.75	117	127 95	245	29	2
21 21	5000	739.6	0.32	1.75	116	127 102	252	30	2
9 22	5230	741.229	0.15	0.80	117	130 101	252	37	2
23 23	5500	742.1	0.23	1.25	109	127 102	252	37	2
10 24	5730	743.963	0.10	0.53	108	135 101	250	30	2
25 25	6000	745.0	0.08	0.42	107	125 102	250	38	2
and	6230	746.107							
Leak check: .023 → .033 = .010 per ft pitot + v ₂ 3.5 pitot - v ₂ 3.7 49.943 .5945 2.3128 117.44 102.90									

Plant Louisiana Pacific -
 Sampling Location MDF RTO duct
 Test For PM/NOx/CO
 Test Operators Russell/Moore

RUN No. 2
 Date 1-18-94
 Time start 1656 end 1809

Meter Box LAC 591249
 Sample Box No. 4
 Probe/Pitot 6.55
 Pitot Cp .84
 Nozzle Dia. .272 ss
 Filter No. _____
 Amb. Temp. °F 30
 Bar. Press. "Hg 29.25
 Static Press. "H₂O -1.6

No. Sample Pts. 5 x 5
 Minutes/Pt. 2.5
 NOMOGRAPH
 ΔH@ 1.85
 Meter Temp. _____
 % H₂O _____
 C-Factor _____
 Stack Temp. _____
 Ref. ΔP _____

Gas Analysis DRSATT
 CO₂ 1.0
 O₂ 19.8
 CO _____
 Time _____
 Condensate:
 tare 200 fin 261
 Silica gel:
 tare _____ fin 3.5

Remarks: _____

Port Point	El. Time, Min.	DGM Reading, Ft. ³	Velocity Head ΔP, in. H ₂ O	Orifice ΔH in. H ₂ O	Stack Temp. °F	Meter Temp., °F In	Meter Temp., °F Out	Oven Temp. °F	Imp. Temp. °F	Vac. in. Hg
1 1	000	746.453	0.75	4.10	117	92	70	248	35	3
2 2	230	749.6	0.89	5.00	118	101	94	244	35	3
3 3	500	752.5	0.15	6.20	121	106	93	245	35	3
2 4	730	755.789	0.60	3.25	117	112	96	251	35	3
5 5	1000	758.3	0.36	1.95	119	117	96	250	35	3
6 6	1230	760.2	0.57	3.20	119	118	95	253	36	3
3 7	1500	762.202	0.22	1.20	118	118	96	251	35	3
8 8	1730	763.6	0.19	1.05	120	119	96	247	35	3
9 9	2000	765.300	0.30	1.60	120	120	96	246	35	3
4 10	2230	766.309	0.08	0.43	119	117	97	251	35	3
11 11	2500	767.5	0.08	0.43	116	118	94	252	35	3
12 12	2730	768.9	0.25	1.35	113	115	99	252	35	3
5 13	3000	769.700	0.06	0.32	115	114	96	247	35	3
14 14	3230	770.6	0.06	0.32	114	114	98	247	35	3
15 15	3500	771.4	0.05	0.28	106	115	100	250	35	3
6 16	3730	772.214	1.00	5.50	117	116	96	250	35	3
17 17	4000	775.7	1.10	6.00	122	121	101	250	33	3
7 18	4230	778.802	0.74	4.00	121	126	99	248	35	3
19 19	4500	782.1	0.63	3.50	121	133	104	251	34	3
8 20	4730	784.607	0.30	1.60	119	131	104	251	34	3
21 21	5000	786.5	0.33	1.75	119	121	105	250	34	3
9 22	5230	788.343	0.13	0.70	118	132	102	250	34	3
23 23	5500	789.7	0.21	1.20	119	129	103	251	34	3
10 24	5730	790.999	0.10	0.53	118	127	103	250	35	2
25 25	6000	792.1	0.10	0.53	118	128	104	250	35	2
and 26	6230	793.246								
27										
28										
29										
30										
31										
32										
33										
34										
35										

back check: 074 → 0 29 = 00542 9 "H₂
 pitot - ve 51
 pitot - ve 6.2
 46.843 .5808 2.2436 117.60 108.52

PARTICULATE CATCH ANALYSIS

SAMPLES: L.P. - Urania M.O.F. / Dryer RTO Inlet
 DATE TAKEN: 1-18-94 DATE ANALYZED: 1-23-94
 DELIVERED BY: DER RECEIVED BY: DER
 ANALYZED BY: DER

(Attach chain of custody if additional exchanges occur)

FILTERS:

RUN NO.	1	2	3	
FILTER NO.	531	534	536	
FILTER TARE, gms.	.5628	.5599	.5623	
	.6342	.8157	.6340	
	.6343	.8156	.6344	
FINAL WEIGHT, gms.	.6343	.8156	.6344	
NET GAIN, gms.	.0715	.2557	.0721	

PROBE WASH:

RUN NO.	1	2	3	
CONTAINER I.D.	DRY NR 1	DRY NR 2	DRY NR 3	
VOLUME INTACT?	✓	✓	✓	
VOLUME, ml	175	160	200	
TARE WEIGHT, gms.	(69) 112.5819	(71) 115.8177	(83) 105.1028	
	112.5920	115.9137	105.1212	
	112.5917	115.9130	105.1211	
		115.9131		
FINAL WEIGHT, gms.	112.5917	115.9131	105.1211	
NET GAIN, gms.	.0098	.0954	.0183	
LESS BLANK, gms.				

PARTICULATE SAMPLE WEIGHT:

RUN NO.	1	2	3	
filter + probe, mg.	81.3	351.1	90.4	

PARTICULATE CATCH ANALYSIS

(Back Half Methylene Chloride Extraction)

SAMPLES:

LP. - Dryers RTO Heat

DATE TAKEN:

1-18-94

DATE ANALYZED:

1-26-94

DELIVERED BY:

DR

RECEIVED BY:

DR

ANALYZED BY:

DR

(Attach chain of custody if additional exchanges occur)

AQUEOUS FRACTION:

RUN NO.	1	2	3	
CONTAINER I.D.	DRY N R1 BAK	DRY N R2 BAK	DRY N R3 BAK	
VOLUME INTACT?	✓	✓	✓	
VOLUME, ml	330	350	350	
TARE WEIGHT, gms.	(90) 98.6677	(68) 112.5339	(83) 105.1028	
	98.6690	112.5371	105.1076	
	98.6686	112.5369	105.1084	
			105.1083	
FINAL WEIGHT, gms.	98.6686	112.5369	105.1083	
NET GAIN, gms.	.0019	.0030	.0055	0
LESS BLANK, gms.				

ORGANIC FRACTION

RUN NO.	1	2	3	
CONTAINER I.D.				
VOLUME INTACT?	✓	✓	✓	
VOLUME, ml				
TARE WEIGHT, gms.	(56) 105.8160	(62) 113.2209	(85) 109.1492	
	105.8186	113.2266	109.1548	
	105.8187	113.2261	109.1547	
FINAL WEIGHT, gms.	105.8187	113.2261	109.1547	
NET GAIN, gms.	.0027	.0052	.0055	0
LESS BLANK, gms.				

PARTICULATE SAMPLE WEIGHT:

RUN NO.	1	2	3	
PQ	1.9	3.0	3.5	
OR	2.7	5.2	5.5	

MDF DRYERS

RTO INLET

VOC/HCOH INLET LOADING TEST

Plant Louisiana Pacific - Umana MDF
 Sampling Location Bayou D RTO Indst
 Test For PICOH/VOC
 Test Operators Russell / Mann

RUN No. 1
 Date 1-19-94
 Time start 1105 end 1511

Meter Box RAC 591349
 Sample Box N-4
 Probe/Pitot 6' Teflon
 Pitot Cp 84
 Nozzle Dia. 1/80 in
 Filter No. N/A

No. Sample Pts. 5x5
 Minutes/Pt. 2.5

NOMOGRAPH
 $\Delta H @$ 1.85
 Meter Temp. 100
 % H₂O 10
 C-Factor 1.0
 Stack Temp. 120
 Ref. ΔP .42

Gas Analysis Eg-7
 CO₂ 1.0 1.0 1.0
 O₂ 5.0 9.8
 CO _____
 Time _____

Condensate:
 tare Ran fin _____
 Silica gel:
 tare _____ fin _____

Remarks:
 1) DNPH 562.5 601.5
 2) DNPH 570.0 579.5
 3) MT 482.0 482.5
 4) S.Gel 780.5 786.0
Bayou D RTO Indst
point 1236 Mann
0.260
0.260 { 260 g/m³
0.266

Port Point	El. Time, Min.	DGM Reading, Ft. ³	Velocity Head ΔP , in. H ₂ O	Orifice ΔH in. H ₂ O	Stack Temp. °F	Meter Temp., °F In Out	Oven Temp. °F	Imp. Temp. °F	Vac in. Hg
1 1	0.00	793.664	0.70	3.10	132	70 69	N/A	36	2
2	230	796.5	0.98	4.40	129	74 67		35	2
3	500	798.7	1.15	5.20	128	75 71		35	2
2 4	730	801.855	0.45	1.95	134	81 69		35	2
5	1000	803.7	0.40	1.75	136	89 70		38	2
6	1230	805.7	0.55	2.40	131	93 72		39	2
3 7	1500	807.6	0.18	0.80	133	103 79		39	2
8	1730	809.3	0.17	0.75	135	98 74		39	2
9	2000	810.6	0.35	1.55	129	99 78		40	2
4 10	2230	812.125	0.68	0.33	133	98 77		40	2
11	2500	812.9	0.10	0.45	135	102 79		40	2
12	2730	813.8	0.22	0.90	134	101 80		40	2
5 13	3000	814.152	0.10	0.44	131	75 73		39	2
14	3230	815.0	0.08	0.33	128	76 74		39	2
15	3500	815.9	0.06	0.26	128	77 74		40	2
6 16	3730	816.532	1.25	5.50	137	80 77		42	2
17	4000	819.6	1.25	5.50	140	86 78		42	2
7 18	4230	823.000	0.83	3.70	136	95 80		43	2
19	4500	825.6	0.64	2.80	138	98 84		43	2
8 20	4730	827.910	0.37	1.65	140	104 81		47	2
21	5000	829.7	0.36	1.60	138	107 83		50	2
9 22	5230	831.431	0.25	1.10	143	107 83		50	2
23	5500	833.0	0.24	1.05	136	107 84		50	2
10 24	5730	834.411	0.14	0.60	137	111 85		50	2
25	6000	835.7	0.18	0.84	129	109 85		51	2
26	6230	837.258							

Leak check: 056 $\rightarrow$ 0.056 = 0.000 g/c 11 11/4
 pitot + vc 4.9
 pitot - vc 6.0

A3.594 6089 1.9580 133.20 84.80

Plant Louisiana Pacific - Wrentham Louisiana MDF
 Sampling Location MDF RTD T&E
 Test For PM10, PM2.5, HCOM, VOC
 Test Operators Russell

RUN No. 2
 Date 1-19-94
 Time start 1626 end 1727

Meter Box RALS91349
 Sample Box 14.4
 Probe/Pitot 6" t/pt
 Pitot Cp
 Nozzle Dia. .277 g/as
 Filter No.
 Amb. Temp. °F 40
 Bar. Press. "Hg 29.28
 Static Press. "H₂O -1.6

No. Sample Pts. 5x5
 Minutes/Pt. 2.5
 NOMOGRAPH
 ΔH@ 1.85
 Meter Temp. 100
 % H₂O 100%
 C-Factor 10.0
 Stack Temp. 125
 Ref. ΔP .33

Gas Analysis Aspirate
 CO₂ 1.0
 O₂ 19.7
 CO
 Time
 Condensate:
 tare 30.00 fin
 Silica gel:
 tare fin

Remarks:
imperial Tare Final
 1) DNPH 566.5 627.0
 2) DNPH 575.5 593
 3) AT 482.5 483.5
 4) SC-1 758.5 779.0
 ① .277
 ② .277
 ③ .277

Port Point	El. Time, Min.	DGM Reading, Ft. ³	Velocity Head ΔP, in. H ₂ O	Orifice Δ H in. H ₂ O	Stack Temp. °F	Meter Temp., °F		Oven Temp. °F	Imp. Temp. °F	Vac in. Hg
						In	Out			
1 1	000	837.685	0.65	3.60	134	88	86	N/A	40	2
2	230	840.3	0.83	4.70	138	90	87		43	2
3	500	843.3	0.85	6.60	136	93	87		45	2
2 4	730	846.557	0.58	2.80	139	100	89		45	3
5	1000	849.1	0.36	2.00	138	107	89		45	2
6	1230	851.1	0.45	2.45	139	108	90		44	2
3 7	1500	853.120	0.29	1.60	137	111	93		45	2
8	1730	855.0	0.22	1.20	140	112	92		45	2
9	2000	856.7	0.27	1.50	138	113	92		45	2
4 10	2230	858.298	0.13	0.72	136	113	94		45	2
11	2500	859.6	0.08	0.44	135	114	91		45	2
12	2730	860.7	0.17	0.90	127	116	96		45	2
5 13	3000	861.916	0.07	0.38	125	116	95		45	2
14	3230	863.0	0.07	0.38	131	116	96		48	2
15	3500	864.0	0.06	0.33	113	117	98		50	2
6 16	3730	864.899	1.25	7.00	134	115	103		53	5
17	4000	868.3	1.25	7.00	138	118	100		55	5
7 18	4230	872.142	1.00	5.60	137	127	100		55	5
19	4500	875.6	0.61	3.40	138	132	101		55	5
8 20	4730	878.094	0.33	1.85	135	133	102		52	3
21	5000	880.2	0.31	1.70	136	125	106		52	3
9 22	5230	881.806	0.11	0.65	140	133	104		52	3
23	5500	883.0	0.18	1.05	138	129	104		52	3
10 24	5730	884.500	0.12	0.65	125	125	108		50	2
25	6000	885.8	0.12	0.65	138	128	104		50	2
and	6230	886.942								

back check: .085 → .085 = .000 cfm @ "1/2"
 pitot + ve 7.7
 pitot - ve 7.0

49.257

.5910

2.3460

134.60

105.60

Plant L.P. - Union M.D.F.
 Sampling Location MDF RTU Inlet
 Test For HCOH/VOC
 Test Operators Russell / mmm

RUN No. 3
 Date 1-19-94
 Time start 1812 and 1921

Meter Box RACS9139
 Sample Box NO. 4
 Probe/Pitot 6' tpa
 Pitot Cp 84
 Nozzle Dia. .277 g/a
 Filter No. _____

No. Sample Pts. 25x5
 Minutes/Pt. 2.5
 NOMOGRAPH
 $\Delta H @$ 1.85
 Meter Temp. _____
 % H₂O _____
 C-Factor _____
 Stack Temp. _____
 Ref. ΔP .33

Gas Analysis Fyate
 CO₂ 1.0
 O₂ 19.8
 CO _____
 Time _____
 Condensate:
 tare Romaka fin _____
 Silica gel:
 tare Romaka fin _____

Remarks: Turn Fuel
 1) DMPH 562.0 / 625.0
 2) DMPH 577.0 / 596.5
 3) MT 482.5 / 483.5
 4) S. Gel 779.0 / 787

Amb. Temp. °F 38
 Bar. Press. "Hg 30.28
 Static Press. "H₂O -1.6

Port Point	El. Time, Min.	DGM Reading, Ft. ³	Velocity Head ΔP , in. H ₂ O	Orifice ΔH in. H ₂ O	Stack Temp. °F	Meter Temp., °F In	Meter Temp., °F Out	Oven Temp. °F	Imp. Temp. °F	Vac. in. Hg
1	1	200	887.216	0.96	5.50	132	98	97	40	5
2	2	230	890.4	1.05	5.90	133	102	97	37	5
3	3	500	893.8	1.10	6.20	133	106	96	46	6
4	4	730	897.062	0.54	3.00	135	109	97	45	3
5	5	1000	899.7	0.33	1.80	131	120	97	45	3
6	6	1230	901.6	0.54	3.00	131	121	97	43	3
7	7	1500	903.743	0.25	1.35	133	124	100	43	3
8	8	1730	905.7	0.21	1.15	133	123	98	44	3
9	9	2000	906.9	0.24	1.30	129	121	98	40	2
10	10	2230	908.370	0.12	0.65	127	122	98	40	2
11	11	2500	909.6	0.13	0.71	133	123	100	41	2
12	12	2730	910.8	0.15	0.84	118	125	99	40	2
13	13	3000	912.001	0.08	0.46	125	121	100	41	2
14	14	3230	913.1	0.09	0.50	129	122	99	41	2
15	15	3500	914.2	0.08	0.46	128	122	101	41	2
16	16	3730	915.039	0.10	0.62	140	117	100	40	6
17	17	4000	918.3	1.10	6.20	142	123	101	40	6
18	18	4230	921.783	0.69	3.90	138	128	101	39	6
19	19	4500	925.1	0.63	3.50	142	135	103	40	6
20	20	4730	927.169	0.38	2.10	137	132	103	39	3
21	21	5000	929.7	0.31	1.70	141	137	107	46	3
22	22	5230	931.172	0.20	1.10	129	132	106	46	3
23	23	5500	932.7	0.27	1.50	127	132	109	42	3
24	24	5730	934.3	0.09	0.50	126	129	107	39	2
25	25	6000	935.6	0.10	0.60	133	130	107	38	2
end	6230	936.651								

Leak Check: .013
 pitot + $\sqrt{e}$ 3.2
 pitot - $\sqrt{e}$ 7.1

49.435

5994

2.3916

132.20

111.44

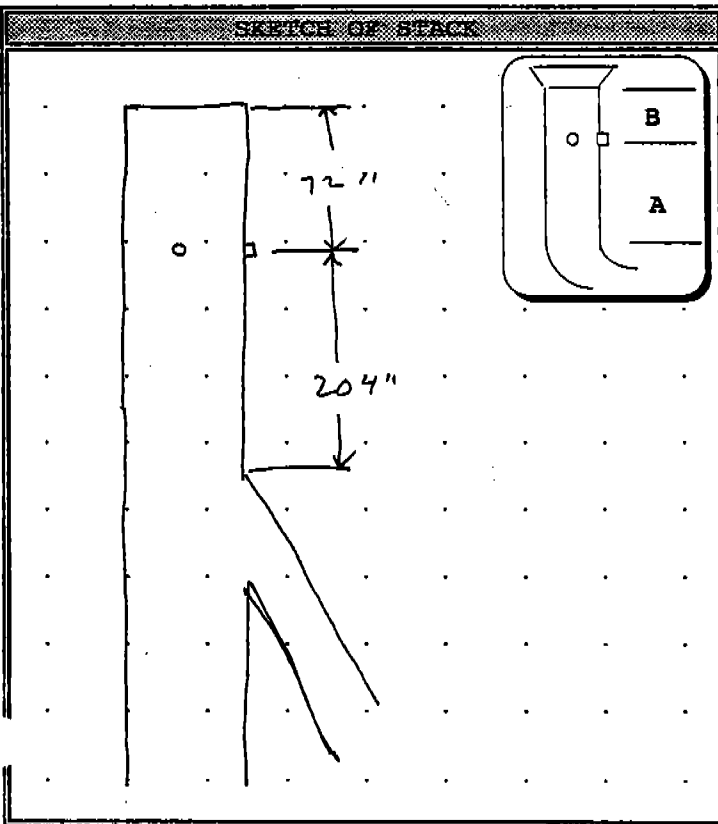
PRESS VENT RTO

PM/CO/NO_x EMISSIONS TEST

STACK CONFIGURATION AND SAMPLE POINT LAYOUT FOR CIRCULAR STACKS

PLANT: L.P. - Maria M D F
SOURCE: Press Vent RTO Outlet
TEST FOR: Ph set up
TEST OPERATORS: Russell

Date: 1-19-94

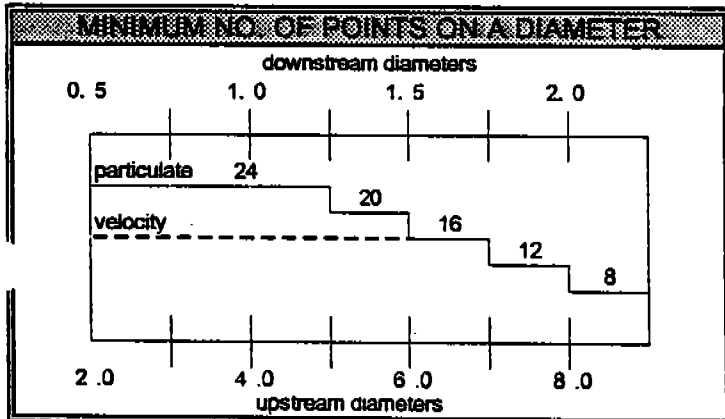


PERCENT OF DIAMETER								
points on a diameter								
point no.	2	4	6	8	10	12	14	16
1	14.6	6.7	4.4	3.2	2.6	2.1	1.8	1.6
2	85.4	25.0	14.6	10.5	8.2	6.7	5.7	4.9
3	75.0	29.6	19.4	14.6	11.8	9.9	8.5	
4	93.3	70.4	32.3	22.6	17.7	14.6	12.5	
5	85.4	67.7	34.2	25.0	20.1	16.9		
6	95.6	80.6	65.8	35.6	26.9	22.0		
7	89.5	77.4	64.4	36.6	28.3			
8	96.8	85.4	75.0	63.4	37.5			
9	91.8	82.3	73.1	62.6				
10	97.4	88.2	79.9	71.7				
11	93.3	85.4	78.0					
12	97.9	90.1	83.1					
13	94.3	87.5						
14	98.2	91.5						
15	95.1							
16	98.4							

Point No.	Inches from wall	velocity head
1	1.4	
2	4.4	
3	7.7	
4	11.6	
5	16.4	
6	23.3	
7	42.2	
8	49.1	
9	53.9	
10	57.8	
11	61.1	
12	63.8	

Pitot ID : Pitot Cp: Stack Temp:

Remarks:



Pitot ID : Pitot Cp: Stack Temp:

Plant Louisiana Pacific - Uraia MDFSampling Location MDF Phase RTO outletTest For HCN/CO/NOxTest Operators Raney/McKnightRUN No. 1Date 1-21-94Time start 0818 and 0921

Meter Box Anderson
 Sample Box 3
 Probe/Pitot 6' teflon
 Pitot Cp .87
 Nozzle Dia. .266 glass
 Filter No. _____

No. Sample Pts. 12 x 2
 Minutes/Pt. 2.5
 NOMOGRAPH
 $\Delta H @$ 1.80
 Meter Temp. 100
 % H₂O 10
 C-Factor .96
 Stack Temp. 230
 Ref. ΔP .45

Gas Analysis int. BAG
 CO₂ 0
 O₂ 20.9 - 5 max
 CO _____
 Time _____

Condensate:
 tare 200 fin 209
 Silica gel:
 tare _____ fin +9

Remarks:
Nozzle (glass)
Ø .266
Ø .266
Ø .266

Amb. Temp. °F 96
 Bar. Press. "Hg 30.31
 Static Press. "H₂O -50

Port Point	El. Time, Min.	DGM Reading, Ft.	Velocity Head ΔP , in. H ₂ O	Orifice ΔH , in. H ₂ O	Stack Temp. °F	Meter Temp., °F In Out	Oven Temp. °F	Imp. Temp. °F	Vac in. Hg
1	0.00	941.310	1.30	5.50	214	57 57	244	40	5
2	2.30	947.5	1.30	5.50	192	70 58	245	40	5
3	5.00	947.0	1.30	5.50	193	79 58	254	41	5
4	7.30	949.9	1.35	5.70	182	87 60	253	41	5
5	10.00	953.1	1.30	5.50	185	95 62	251	40	5
6	12.30	956.4	1.40	6.00	181	101 64	252	38	5
7	15.00	959.0	0.86	3.60	181	104 66	255	38	5
8	17.30	962.0	0.77	3.20	185	105 68	245	40	5
9	20.00	964.2	0.79	3.30	174	106 71	250	40	5
10	22.30	966.7	0.79	3.30	187	108 73	245	40	5
11	25.00	969.6	0.74	3.10	196	110 75	247	39	4
12	27.30	972.0	0.75	3.20	208	111 78	251	38	4
13									
14	30.00	974.210	1.40	5.90	195	106 79	253	40	5
15	2.30	977.4	1.40	6.00	194	116 81	245	40	5
16	5.00	980.3	1.50	6.30	192	117 82	251	40	5
17	7.30	983.8	1.60	6.60	203	123 84	250	40	5
18	10.00	987.7	1.50	6.40	205	126 86	254	40	5
19	12.30	990.7	1.50	6.40	209	127 88	245	40	6
20	15.00	994.5	1.05	4.30	197	129 90	253	40	6
21	17.30	997.9	1.00	4.20	183	125 91	254	40	5
22	20.00	1000.5	0.74	3.90	187	127 91	255	40	5
23	22.30	1002.7	1.00	4.20	210	124 92	248	40	5
24	25.00	1005.8	0.95	4.00	204	124 93	242	41	5
25	27.30	1008.7	1.05	4.40	192	126 93	246	42	5
26	6.00	011.274							

Leak check: .099 → .105 = .006 gpm @ 19" Hg
 pitot +ve 4.0
 pitot -ve 4.0

69.964 1.0631 4.8333 193.88 92.58

Plant Louisiana Pacific - Urethane MDE
 Sampling Location MDE 1 Pen Vent RTO Duct
 Test For PM/CO/NOx
 Test Operators Barney/more mcknight

RUN No. 2
 Date 1-21-94
 Time start 1001 and 1102

Meter Box Anderson
 Sample Box No. 3
 Probe/Pitot 6' Efflu
 Pitot Cp .45
 Nozzle Dia. 2.16
 Filter No.
 Amb. Temp. °F 40
 Bar. Press. "Hg 30.31
 Static Press. "H₂O -50

No. Sample Pts. 12x2
 Minutes/Pt. 2.5
 NOMOGRAPH
 ΔH@ 1.8
 Meter Temp.
 % H₂O
 C-Factor
 Stack Temp.
 Ref. ΔP .45

Gas Analysis int. bag
 CO₂ 0
 O₂ 5 max = 20.9
 CO
 Time
 Condensate:
 tare 200 fin 214
 Silica gel:
 tare fin +6.5

Remarks:

Port Point	El. Time, Min.	DGM Reading, Ft.	Velocity Head ΔP, in. H ₂ O	Orifice ΔH in. H ₂ O	Stack Temp. °F	Meter Temp., °F In	Meter Temp., °F Out	Oven Temp. °F	Imp. Temp. °F	Vac in. Hg
1	000	011.953	1.30	5.50	211	71	71	252	40	5
2	020	014.6	1.20	5.00	202	79	72	250	40	5
3	500	018.6	1.40	6.00	182	93	71	250	41	6
4	730	021.2	1.30	5.50	181	100	72	251	41	6
5	1000	024.7	1.30	5.50	207	104	73	253	41	6
6	1230	027.0	1.30	5.50	188	110	75	257	40	6
7	1500	030.3	0.86	3.60	185	114	77	256	40	6
8	1730	032.9	0.82	3.45	191	114	80	256	40	4
9	2000	035.7	0.72	3.00	186	115	82	256	40	4
10	2230	039.2	0.72	3.00	194	115	84	260	40	4
11	2500	040.3	0.70	2.95	212	117	87	250	40	4
12	2730	042.3	0.72	3.00	189	117	88	244	41	4
13										
14	3000	044.634	1.50	6.30	196	111	89	245	40	6
15	230	048.7	1.50	6.30	192	123	90	256	40	6
16	500	051.5	1.60	6.60	208	128	91	257	40	6
17	730	054.9	1.60	6.60	202	132	93	251	40	6
18	1000	058.4	1.50	6.30	196	133	95	251	40	6
19	1230	062.0	1.45	6.20	199	134	96	250	40	6
20	1500	065.3	1.05	4.40	216	135	98	250	40	6
21	1730	068.4	0.93	3.95	224	133	98	253	40	6
22	2000	071.6	0.99	4.15	191	131	101	246	40	6
23	2230	073.8	0.94	4.00	206	131	101	254	40	6
24	2500	077.3	0.80	3.40	196	131	101	247	40	6
25	2730	079.5	0.75	3.20	196	129	101	251	40	6
26	and 60	082.057								

back check: .073 → .043 = 0.000 g/c 10" H₂O

pitot + ve 5.0
 pitot - ve 5.0
 10.104 1.0490 4.7250 197.92 101.79

Plant Louisiana Pacific
 Sampling Location MOEP line 11ENT RTD Outlet
 Test For 11ENT / PM / CO / NO_x
 Test Operators Russell McKnight

RUN No. 3
 Date 1-21-74
 Time start 1226 end 1227

Meter Box Anderson
 Sample Box No. 2
 Probe/Pitot 6" tip
 Pitot Cp 1.81
 Nozzle Dia. 2.66 in
 Filter No. _____
 Amb. Temp. °F 45
 Bar. Press. "Hg 30.31
 Static Press. "H₂O -5.0

No. Sample Pts. 12x2
 Minutes/Pt. 2.5
 NOMOGRAPH
 ΔH@ 1.8
 Meter Temp. _____
 % H₂O _____
 C-Factor _____
 Stack Temp. _____
 Ref. ΔP .45

Gas Analysis intake
 CO₂ 0
 O₂ SNEX = 20.9
 CO _____
 Time _____
 Condensate:
 tare 200 fin 215
 Silica gel:
 tare _____ fin 19.0

Remarks: _____

Port Point	El. Time, Min.	DGM Reading, Ft.	Velocity Head ΔP, in. H ₂ O	Orifice ΔH in. H ₂ O	Stack Temp. °F	Meter Temp., °F In	Meter Temp., °F Out	Oven Temp. °F	Imp. Temp. °F	Vac in. Hg
1	0.00	082.531	1.40	6.00	207	89	80	252	39	7
2	2.30	085.6	1.50	6.20	207	98	85	251	70	7
3	5.00	088.0	1.55	6.60	215	106	85	250	37	7
4	7.30	091.3	1.50	6.20	219	113	85	250	40	7
5	10.00	095.2	1.50	6.20	215	119	87	250	40	7
6	12.30	098.6	1.40	6.00	199	123	87	252	41	7
7	15.00	102.3	0.83	3.50	209	125	89	250	41	7
8	17.30	105.3	0.78	3.30	194	124	90	247	40	5
9	20.00	107.5	0.77	3.20	199	125	92	250	40	5
10	22.30	110.0	0.73	3.05	201	124	93	265	41	5
11	25.00	112.4	0.75	3.10	205	124	94	260	40	5
12	27.30	114.9	0.75	3.10	190	123	94	260	40	5
13										
14	30.00	117.386	1.45	6.20	198	118	95	244	41	8
15	2.30	120.4	1.60	6.80	230	127	96	257	42	8
16	5.00	124.2	1.50	6.20	197	134	97	250	42	8
17	7.30	127.8	1.55	6.50	203	136	98	255	40	8
18	10.00	130.9	1.60	6.80	198	138	99	251	40	8
19	12.30	134.7	1.40	6.00	221	138	101	252	40	8
20	15.00	137.7	1.00	4.20	202	137	100	256	41	8
21	17.30	140.4	0.96	4.00	215	136	104	255	41	8
22	20.00	143.6	1.00	4.20	221	136	105	255	40	7
23	22.30	146.6	0.77	3.20	224	136	105	256	41	5
24	25.00	148.7	0.78	3.25	220	135	105	251	40	5
25	27.30	151.4	0.75	2.70	202	135	105	247	40	5
26	30.00	153.651								

Leak check: .042
 pitot + 16.2
 pitot - 16.0

71.120

1.0557

4.8542

207.94

110.00

PARTICULATE CATCH ANALYSIS

SAMPLES: L.P. - 1/2 in MAF / Prime Vent RTO outlet
 DATE TAKEN: 1-21-94 DATE ANALYZED: 1-23-94
 DELIVERED BY: DR RECEIVED BY: DR
 ANALYZED BY: DR

(Attach chain of custody if additional exchanges occur)

FILTERS:

RUN NO.	1	2	3	
FILTER NO.	537	539	501	
FILTER TARE, gms.	.5638	.5595	.5650	
	.5633	.5597	.5647	
	.5632	.5597	.5647	
FINAL WEIGHT, gms.	.5632	.5597	.5647	
NET GAIN, gms.	-.0006	0.0002	-0.0003	

PROBE WASH:

RUN NO.	1	2	3	
CONTAINER I.D.	PV R1	PV R2	PV R3	
VOLUME INTACT?	✓	✓	✓	
VOLUME, ml	140	150	150	
TARE WEIGHT, gms.	(3) 104.6267	(7) 111.5432	(90) 107.9579	
	104.6298	111.5437	107.9601	
	104.6299	111.5433	107.9598	
FINAL WEIGHT, gms.	104.6299	111.5433	107.9598	
NET GAIN, gms.	.0032	.0001	.0019	
LESS BLANK, gms.	-0-	-0-	-0-	

PARTICULATE SAMPLE WEIGHT:

RUN NO.	1	2	3	
filter + probe, mg.	2.6	0.3	1.6	

PARTICULATE CATCH ANALYSIS

(Back Half Methylene Chloride Extraction)

SAMPLES:

L.P. Penn Vent RTO (outlet)

DATE TAKEN:

1-21-94

DATE ANALYZED:

1-26-94

DELIVERED BY:

PCR

RECEIVED BY:

PCR

ANALYZED BY:

PCR

(Attach chain of custody if additional exchanges occur)

AQUEOUS FRACTION:

RUN NO.	1	2	3	
CONTAINER I.D.	PUR1 BAK	PUR2 BAK	PUR3 BAK	
VOLUME INTACT?	✓	✓	✓	
VOLUME, ml	300	300	300	
TARE WEIGHT, gms	(25) 97.0868	(29) 98.3928	108.5425(88)	
	97.0871	98.3932	108.5429	
	97.0871	98.3930	108.5433	
FINAL WEIGHT, gms	97.0871	98.3930	108.5433	
NET GAIN, gms	10003	10002	10008	
LESS BLANK, gms				

ORGANIC FRACTION

RUN NO.	1	2	3	
CONTAINER I.D.	same			
VOLUME INTACT?	same			
VOLUME, ml	same			
TARE WEIGHT, gms	(7) 111.5410	(81) 104.6007	(89) 106.4080	
	111.5410	104.6014	106.4085	
	111.5411	104.6010	106.4087	
FINAL WEIGHT, gms	111.5411	104.6010	106.4087	
NET GAIN, gms	.0001	.0009	.0007	
LESS BLANK, gms				

PARTICULATE SAMPLE WEIGHT:

RUN NO.	1	2	3	
Aqueous	0.3	0.2	0.4	
Aqueous fraction, mg	0.1	0.9	0.7	

ORGANIC

PRESS VENT RTO

VOC/HCOH EMISSIONS TEST

Plant Louisiana Pacific - Urethane Louisiana MIF
 Sampling Location MDF Pura RTO Outlet
 Test For HCOH/VOC
 Test Operators Russell / mone

RUN No. 1
 Date 1-20-94
 Time start 1241 end 1242

Meter Box Anderson
 Sample Box 123
 Probe/Pitot 6' teflon
 Pitot Cp .84
 Nozzle Dia. .2185 in.
 Filter No.

No. Sample Pts. 12x2
 Minutes/Pt. 2.5
 NOMOGRAPH
 $\Delta H @$ 1.85
 Meter Temp. 100
 % H₂O 10
 C-Factor .96
 Stack Temp. 200
 Ref. ΔP 1.05

Gas Analysis int. BAG
 CO₂ 0
 O₂ Servoex = 20.9
 CO
 Time
 Condensate:
 tare Russell fin 16.5
 Silica gel:
 tare fin

Remarks:
imaging system final
 1) DNPH 577.0 585.0
 2) DNPH 577.0 580.0
 3) MT 478.0 478.5
 4) S.Gol 731.5 736.3
 5) 2.18
 6) 2.18
 7) 2.18

Amb. Temp. °F 47
 Bar. Press. "Hg 29.29
 Static Press. "H₂O -.50

Port Point	El. Time, Min.	DGM Reading, Ft. ³	Velocity Head ΔP , in. H ₂ O	Orifice ΔH , in. H ₂ O	Stack Temp. °F	Meter Temp., °F In Out	Oven Temp. °F	Imp. Temp. °F	Vac. in. Hg
1	000	791.977	1.25	2.20	221	63 61	N/A	42	2
2	230	793.8	1.25	2.20	217	66 61		42	2
3	500	795.6	1.35	2.40	199	68 62		40	2
4	730	797.4	1.30	2.15	203	78 63		40	2
5	1000	799.5	1.40	2.50	199	83 64		40	2
6	1230	801.5	1.20	2.30	213	88 65		43	2
7	1600	803.8	0.85	1.50	207	94 67		44	2
8	1730	805.3	0.71	1.30	207	93 68		45	2
9	2000	807.1	0.77	1.35	205	93 70		46	2
10	2230	808.5	0.72	1.25	199	94 71		46	2
11	2500	809.9	0.70	1.20	206	95 72		46	2
12	2730	812.8	0.56	1.00	202	97 75		46	2
13									
14	3000	813.200	1.40	2.50	222	95 76		46	2
15	230	815.5	1.60	2.80	210	104 78		46	2
16	500	817.7	1.60	2.80	217	109 80		46	2
17	730	820.1	1.60	2.80	226	112 81		46	2
18	1000	822.2	1.50	2.60	216	114 82		46	2
19	1230	824.6	1.50	2.60	221	115 82		49	2
20	1600	826.8	1.10	2.00	205	117 86		44	2
21	1730	828.8	0.94	1.70	202	114 87		45	2
22	2000	828.8	0.95	1.75	220	112 89		45	2
23	2230	832.8	0.73	1.30	242	111 90		45	2
24	2600	834.3	0.77	1.25	211	110 90		45	2
25	2730	835.6	0.82	1.45	203	110 90		45	2
26	2900	837.354							

Leak check: 1.063 - 1.068 = 1005 μ e 8.4/Hg

pitot r = 3.3
 pitot - 3.7

45,377

1.0460

1.9583

211.38

86.38

Plant Louisiana Pacific - Urania MDF
 Sampling Location MDF Press RTO Outlet
 Test For H₂O₂ / VOC
 Test Operators Russell / Moore

RUN No. 2
 Date 1-20-94
 Time start 1400 end 1501

Meter Box Anderson
 Sample Box N-3
 Probe/Pitot 6' Teflon
 Pitot Cp .84
 Nozzle Dia. .218
 Filter No.

No. Sample Pts. 12x2
 Minutes/Pt. 2.5
 NOMOGRAPH
 $\Delta H @$ 1.80
 Meter Temp.
 % H₂O
 C-Factor
 Stack Temp.
 Ref. ΔP 1.05

Gas Analysis Int Bag
 CO₂ 0.1 direct
 O₂ 20.9
 CO
 Time
 Condensate:
 tare Ram fin
 Silica gel:
 tare fin

Remarks:

	Tare	Final
1) DNPH	578.5	588.0
2) DNPH	576.5	577.5
3) MT	478.5	479.5
4) S.Gel	736.7	748.0

22

Port Point	El. Time, Min.	DGM Reading, Ft. ³	Velocity Head ΔP , in. H ₂ O	Orifice ΔH , in. H ₂ O	Stack Temp. °F	Meter Temp., °F In Out	Oven Temp. °F	Imp. Temp. °F	Vac in. Hg
1	000	837.763	1.70	3.00	216	69 68	N/A	47	3
2	230	840.4	1.35	2.40	207	76 67		49	3
3	500	842.3	1.40	2.50	212	81 68		50	3
4	730	844.6	1.50	2.65	216	87 69		50	3
5	1000	846.8	1.85	3.25	215	94 70		53	3
6	1230	848.8	1.80	3.20	238	99 71		53	3
7	600	851.4	1.60	2.80	206	104 73		53	3
8	730	853.5	1.70	3.00	203	107 75		52	3
9	2000	856.0	1.35	2.40	209	109 77		50	3
10	2230	858.1	1.10	2.00	201	109 79		50	3
11	2600	860.1	1.30	2.30	212	109 80		49	3
12	2730	862.2	1.35	2.40	210	111 82		49	3
13									
14	30/100	864.406	2.00	3.60	199	104 83		51	3
15	230	866.9	2.20	4.00	205	115 84		50	3
16	500	869.9	2.10	3.90	238	119 85		50	3
17	730	872.3	2.10	3.90	208	121 87		50	3
18	1000	875.0	1.90	3.40	219	123 89		50	3
19	1230	877.7	2.00	3.60	226	123 90		49	3
20	1500	880.4	1.90	3.40	210	125 92		49	3
21	1730	883.1	1.30	2.30	224	124 93		49	3
22	2000	885.1	1.10	1.95	243	120 94		48	3
23	2230	886.9	1.15	2.10	212	118 94		50	3
24	2500	888.9	0.97	1.70	230	118 95		50	3
25	2730	890.6	1.05	1.85	206	116 95		50	3
26	30/100	892.660							

Leak check: .070 → .075 = .005 up 9" Hg
 pitot - 4.2
 pitot - 3.4

54.897 1.2456 2.8167 216.04 94.60

Plant Louisiana Pacific - Morgan M.D.F.
 Sampling Location M.D.F. Phase RTO Outlet
 Test For H2O/H2O
 Test Operators R. Brown / M. Moore

RUN No. 3

Date 1-20-94

Time start 1600 end 1700

Meter Box Anderson
 Sample Box No. 3
 Probe/Pitot 6" t/flo
 Pitot Cp .84
 Nozzle Dia. .218 gpa
 Filter No.

No. Sample Pts. 12 x 2
 Minutes/Pt. 2.5

NOMOGRAPH

$\Delta H @$ 1.80
 Meter Temp.
 % H₂O
 C-Factor
 Stack Temp.
 Ref. ΔP 1.05

Gas Analysis int. BAS
 CO₂ 0
 O₂ 20.9
 CO
 Time

Condensate:
 tare Ramco fin
 Silica gel:
 tare fin

Remarks:

1) DNPH	577.0	584.5
2) DNPH	579.0	581.0
3) MT	478.5	479.0
4) S. Gel	744.0	750.0

16.0

Port Point	El. Time, Min.	DGM Reading, Ft. ³	Velocity Head ΔP , in. H ₂ O	Orifice ΔH in. H ₂ O	Stack Temp. °F	Meter Temp., °F In Out	Oven Temp. °F	Imp. Temp. °F	Vac in. Hg
1	000	892.642	1.40	2.50	193	76 68	N/A	45	3
2	230	895.8	1.40	2.50	197	77 68		45	3
3	500	897.9	1.35	2.40	231	81 69		45	3
4	730	900.1	1.40	2.50	193	87 69		45	3
5	1000	902.3	1.40	2.50	199	93 71		44	3
6	1230	904.5	1.35	2.40	198	97 72		44	3
7	1500	906.6	0.90	1.60	206	99 73		45	3
8	1730	908.4	0.69	1.20	200	99 74		45	3
9	2000	910.1	0.69	1.20	204	97 76		45	3
10	2230	911.3	0.67	1.20	195	97 76		46	3
11	2500	912.9	0.64	1.15	209	98 78		46	3
12	2730	914.6	0.64	1.15	204	100 79		46	3
13									
1	3000	915.861	0.45	2.55	212	92 80		47	3
2	230	918.1	1.50	2.60	210	107 82		46	3
3	500	920.2	1.55	2.80	211	107 82		46	3
4	730	922.5	1.50	2.65	237	112 83		46	3
5	1000	924.8	1.50	2.60	204	115 85		46	3
6	1230	926.9	1.60	2.80	210	115 86		45	3
7	1500	929.5	1.10	1.95	218	116 88		45	3
8	1730	931.6	0.95	1.70	235	115 88		46	3
9	2000	932.8	1.05	1.90	242	113 89		46	3
10	2230	935.4	0.95	1.70	242	114 90		46	3
11	2500	937.3	0.85	1.50	211	114 90		46	2
12	2730	938.8	0.90	1.60	206	113 91		46	3
end	60	940.741							

Lock check: .065 - .067 = .004 in @ 8" H₂O
 pitot +ve 4.6
 pitot -ve 5.0

47,099

1.0570

2.0271

210.92

107.31

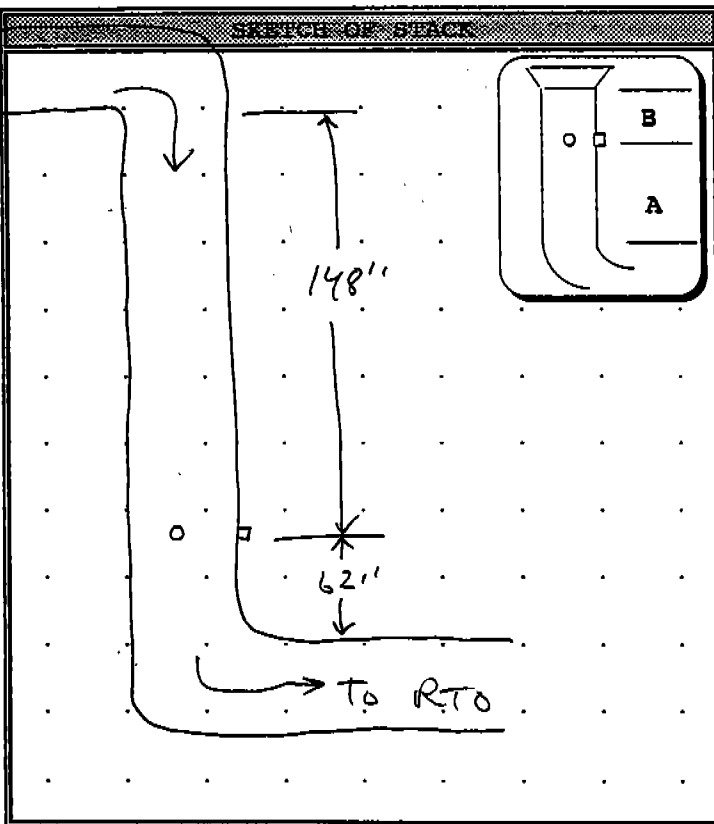
PRESS VENT RTO INLET

PM/CO/NO_x INLET LOADING TEST

STACK CONFIGURATION AND SAMPLE POINT LAYOUT FOR CIRCULAR STACKS

PLANT: L.P. - Urania MOF
SOURCE: PRESERVENT RTO INLET
TEST FOR: PM Set up
TEST OPERATORS: Ramon

Date: 1-19-94



PERCENT OF DIAMETER								
points on a diameter								
point no.	2	4	6	8	10	12	14	16
1	14.6	6.7	4.4	3.2	2.6	2.1	1.8	1.6
2	85.4	25.0	14.6	10.5	8.2	6.7	5.7	4.9
3	75.0	29.6	19.4	14.6	11.8	9.9	8.5	
4	93.3	70.4	32.3	22.6	17.7	14.6	12.5	
5	85.4	67.7	34.2	25.0	20.1	16.9		
6	95.6	80.6	65.8	35.6	26.9	22.0		
7	89.5	77.4	64.4	36.6	28.3			
8	96.8	85.4	75.0	63.4	37.5			
9	91.8	82.3	73.1	62.5				
10	97.4	88.2	79.9	71.7				
11	93.3	85.4	78.0					
12	97.9	90.1	83.1					
13		94.3	87.5					
14		98.2	91.5					
15			95.1					
16			98.4					

STACK DIAMETER: 65.75"

Distance from ports to disturbance:

A. to upstream disturbance

B. to downstream disturbance

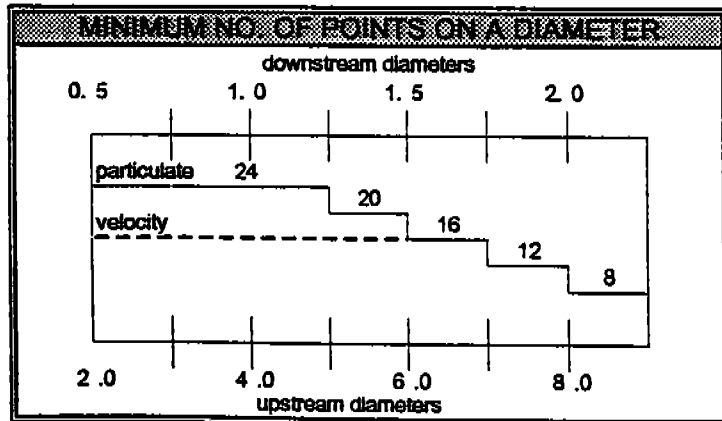
Upstream diameters:

Downstream diameters:

Minimum No. sample points required:

No. sample points selected:

Port Length:

Port Type:**Port Access:**

Point No.	Inches from wall	velocity head
1	1.4	
2	4.4	
3	7.8	
4	11.6	
5	16.4	
6	23.4	
7	42.3	
8	49.3	
9	59.1	
10	58.0	
11	61.3	
12	64.0	

Pitot ID : Pitot Cp: Stack Temp:

Remarks:

[illegible]

Plant Komarine Pacific - Urania MRF
 Sampling Location MRF Pump test RTO Boat
 Test For PM/CO/NOx
 Test Operators Russell/Morre

RUN No. 2
 Date 1-21-97
 Time start 1000 end 1100

Meter Box Anderson
 Sample Box No. 4
 Probe/Pitot 8' flex
 Pitot Cp 84'
 Nozzle Dia. 218
 Filter No.

No. Sample Pts. 12x2
 Minutes/Pt. 2.5
 NOMOGRAPH
 $\Delta H @$ 1.85
 Meter Temp. 100
 % H₂O 610
 C-Factor 1.0
 Stack Temp. 100
 Ref. ΔP .21

Gas Analysis AIR
 CO₂
 O₂
 CO
 Time
 Condensate:
 tare 200 fin 210
 Silica gel:
 tare fin 16.5

Remarks:

Port Point	El. Time, Min.	DGM Reading, Ft. ³	Velocity Head ΔP , in. H ₂ O	Orifice ΔH in. H ₂ O	Stack Temp. °F	Meter Temp., °F In	Meter Temp., °F Out	Oven Temp. °F	Imp. Temp. °F	Vac in. Hg
1	000	145.967	0.57	1.30	75	87	81	247	90	2
2	230	147.6	0.61	1.40	75	92	76	248	29	2
3	500	188.9	0.60	1.35	80	92	77	250	39	2
4	730	191.0	0.60	1.35	80	93	77	270	38	2
5	1000	192.3	0.58	1.30	80	95	78	291	38	2
6	1230	193.7	0.58	1.30	82	94	84	290	38	2
7	1500	195.5	0.85	1.90	83	98	80	251	39	2
8	1730	197.4	0.99	2.25	84	103	81	250	40	2
9	2000	199.3	0.94	2.15	79	105	81	250	40	2
10	2230	201.7	0.95	2.15	80	107	82	250	41	2
11	2500	203.5	0.97	2.20	85	109	82	252	41	2
12	2730	205.1	0.96	2.20	85	114	84	250	42	2
13										
14	3000	207.278	0.82	1.85	86	111	85	243	42	2
15	230	209.2	0.94	2.10	88	110	86	252	42	2
16	500	211.2	0.89	1.95	85	112	85	252	42	2
17	730	213.4	0.75	1.70	85	117	86	252	42	2
18	1000	215.0	0.67	1.50	85	113	88	252	42	2
19	1230	216.5	0.62	1.40	85	113	88	248	41	2
20	1500	218.3	0.58	1.30	85	115	89	252	40	2
21	1730	220.2	0.63	1.40	85	114	87	251	40	2
22	2000	221.6	0.72	1.60	86	120	94	251	40	2
23	2230	223.1	0.67	1.50	87	116	9	252	40	2
24	2500	225.2	0.67	1.50	88	115	89	250	40	2
25	2730	226.5	0.62	1.40	86	122	95	250	40	2
26	3000	228.342								

Leak check: 031 → .035 = .007 cfm
 pitot + ve 4.4
 pitot - ve 3.6

42.375

18564

1.6688

83.29

95.71

Plant Louisiana Pacific - Urdia M.D.F.
 Sampling Location M.D.F. Press RTD Inlet
 Test For Ph/CO/NO_x
 Test Operators Russell / Moore

RUN No. 3
 Date 1-21-94
 Time start 1225 and 1226

Meter Box	<u>RAC</u>	No. Sample Pts.	<u>12 x 2</u>	Gas Analysis	<u>AIR</u>	Remarks:
Sample Box	<u>No. 1</u>	Minutes/Pt.	<u>2.5</u>	CO ₂	_____	
Probe/Pitot	<u>8' Teflon</u>	NOMOGRAPH		O ₂	_____	
Pitot Cp	<u>.87</u>	ΔH@	<u>1.85</u>	CO	_____	
Nozzle Dia.	<u>.218</u>	Meter Temp.	_____	Time	_____	
Filter No.	_____	% H ₂ O	_____	Condensate:		
Amb. Temp. °F	<u>45</u>	C-Factor	_____	tare <u>200</u> fin <u>209</u>		
Bar. Press. "Hg	<u>30.31</u>	Stack Temp.	_____	Silica gel:		
Static Press. "H ₂ O	<u>-2.6</u>	Ref. ΔP	<u>.81</u>	tare _____ fin <u>+3.5</u>		

Port Point	El. Time, Min.	DGM Reading, Ft. ³	Velocity Head ΔP, in. H ₂ O	Orifice ΔH in. H ₂ O	Stack Temp. °F	Meter Temp., °F In	Meter Temp., °F Out	Oven Temp. °F	Imp. Temp. °F	Vac in. Hg
1	0.00	228.611	0.62	1.40	94	93	89	247	44	3
2	23.0	230.5	0.59	1.20	95	94	87	250	40	2
3	5.00	231.9	0.60	1.35	95	90	86	250	40	2
4	7.20	233.5	0.59	1.30	95	97	86	239	41	2
5	12.00	235.2	0.57	1.25	95	99	90	247	41	2
6	12.30	236.9	0.55	1.25	95	102	95	254	40	2
7	15.00	238.7	0.84	1.90	95	101	96	250	40	2
8	17.30	240.4	0.86	1.95	95	114	87	250	40	2
9	20.00	242.1	0.98	2.20	99	111	91	250	40	2
10	22.30	243.9	0.90	2.00	95	112	89	250	41	2
11	25.00	245.8	0.89	2.00	92	113	88	250	40	2
12	27.30	247.7	0.82	1.75	94	113	89	250	40	2
13										
14	30.00	249.592	0.87	1.90	96	117	92	260	42	2
15	23.0	251.5	0.85	1.90	96	115	91	260	42	2
16	5.00	253.4	0.82	1.85	96	115	91	253	40	2
17	7.30	255.5	0.76	1.70	97	114	91	250	40	2
18	5	257.2	0.67	1.50	97	118	91	250	40	2
19	12.20	258.6	0.58	1.30	93	118	96	259	41	2
20	15.00	260.5	0.77	1.70	96	118	93	261	40	2
21	17.30	262.7	0.67	1.50	97	124	95	250	40	2
22	20.00	264.1	0.66	1.50	97	121	96	252	40	2
23	22.30	265.7	0.68	1.50	96	119	94	247	40	3
24	25.00	267.6	0.74	1.70	96	122	96	250	40	3
25	27.30	269.1	0.74	1.70	95	121	95	250	40	3
26	60	270.918								

Leak Check: .050 → .050 = 0.000 4e 9" H₂O
 pitot + ve 26
 pitot - -e 4.5
42.307 .8532 1.6417 95.54 101.08

PARTICULATE CATCH ANALYSIS

SAMPLES:

L.P. - 11/11/94 M.O.F. / Pm V. R.T.O. Inlet

DATE TAKEN:

1-21-94 DATE ANALYZED: 1-23-94

DELIVERED BY:

[Signature] RECEIVED BY: [Signature]

ANALYZED BY:

[Signature]

(Attach chain of custody if additional exchanges occur)

FILTERS:

RUN NO.	1	2	3	
FILTER NO.	538	540	514	
FILTER TARE, gms.	.5593	.5610	.5627	
	.5605	.5649	.5633	
	.5607	.5648	.5635	
FINAL WEIGHT, gms.	.5607	.5648	.5635	
NET GAIN, gms.	.0014	.0038	.0008	

PROBE WASH:

RUN NO.	1	2	3	
CONTAINER I.D.	PVNR1	PVNR2	PVNR3	
VOLUME INTACT?	✓	✓	—	
VOLUME, ml	120	170	140	
TARE WEIGHT, gms.	(2) 104.7530	(62) 113.2218	(11) 102.7996	
	104.7601	113.2258	102.8051	
	104.7599	113.2253	102.8051	
FINAL WEIGHT, gms.	104.7599	113.2253	102.8051	
NET GAIN, gms.	.0069	.0025	.0055	
LESS BLANK, gms.				

PARTICULATE SAMPLE WEIGHT:

RUN NO.	1	2	3	
filter + probe, mg.	8.3	7.3	6.3	

PARTICULATE CATCH ANALYSIS

(Back Half Methylene Chloride Extraction)

SAMPLES:

L.P. Penn Vent RTO Inlet

DATE TAKEN:

1-21-94

DATE ANALYZED:

1-26-94

DELIVERED BY:

DEER

RECEIVED BY:

DEER

ANALYZED BY:

DEER

(Attach chain of custody if additional exchanges occur)

AQUEOUS FRACTION:

RUN NO.	1	2	3	
CONTAINER I.D.	PV NR1 BAK	PV NR2 BAK	PV NR3 BAK	
VOLUME INTACT?	✓	✓	✓	
VOLUME, ml	300	300	300	
TARE WEIGHT, gms.	(3) 104.6240	(15) 107.2502	(90) 107.9644	
	104.6257	107.2538	107.9683	
	104.6257	107.2534	107.9684	
FINAL WEIGHT, gms.	104.6257	107.2534	107.9684	
NET GAIN, gms.	.0017	.0032	.0040	
LESS BLANK, gms.				

ORGANIC FRACTION

RUN NO.	1	2	3	
CONTAINER I.D.	Same			
VOLUME INTACT?	Same			
VOLUME, ml	Same			
TARE WEIGHT, gms.	(69) 112.5820	(90) 107.9573	(91) 102.7999	
	112.5850	107.9609	102.8039	
	112.5841	107.9603	102.8030	
	112.5843	107.9603	102.8028	
FINAL WEIGHT, gms.	112.5843	107.9603	102.8028	
NET GAIN, gms.	.0023	.0030	.0029	
LESS BLANK, gms.				

PARTICULATE SAMPLE WEIGHT:

RUN NO.	1	2	3	
Ag	1.7	3.2	4.0	
ORG Aqueous fraction, mg	2.3	3.0	2.9	

PRESS VENT RTO INLET

VOC/HCOH INLET LOADING TEST

Plant Louisiana Pacific - Vicksburg MDF
 Sampling Location MDF Packer RTO Unit
 Test For HCOH/VOC
 Test Operators Russell / McKnight

RUN No. 1
 Date 1-20-94
 Time start 1140 end 1242

Meter Box RAK
 Sample Box N6.7
 Probe/Pitot 8' t/plan
 Pitot Cp
 Nozzle Dia. 2.260
 Filter No.

No. Sample Pts. 12 x 2
 Minutes/Pt. 2.5
 NOMOGRAPH
 $\Delta H @$ 1.85
 Meter Temp. 100
 % H₂O 4.0
 C-Factor 1.0
 Stack Temp. 400
 Ref. ΔP 38

Gas Analysis Fyite
 CO₂ 0
 O₂ 20.7
 CO
 Time
 Condensate:
 tare Rm fin 0.5
 Silica gel:
 tare Rm fin

Remarks:
Turn final
 1) DMPH 562.5 511.5
 2) DMPH 571.5 572.5
 3) DMPH 492.0 782.5
 4) SAPK 758.0 763.0
 Paul Laird DOEQ

Port Point	El. Time, Min.	DGM Reading, Ft. ³	Velocity Head ΔP , in. H ₂ O	Orifice ΔH , in. H ₂ O	Stack Temp., °F	Meter Temp., °F In Out	Oven Temp., °F	Imp. Temp., °F	Vac in. Hg
1	000	937.421	0.50	2.40	100	65 64	N/A	43	3
2	230	939.5	0.60	2.90	99	65 63		40	3
3	500	942.5	0.57	2.70	97	79 66		40	3
4	730	944.2	0.58	2.80	100	75 64		40	3
5	1000	946.2	0.61	3.00	100	79 66		43	2
6	1230	948.7	0.61	3.00	100	87 66		44	3
7	1500	950.6	0.79	3.60	101	91 62		44	3
8	1730	953.5	0.85	4.10	100	94 68		45	4
9	2000	956.3	0.95	4.60	97	97 69		46	4
10	2230	959.0	0.99	4.80	102	101 70		46	4
11	2500	961.9	0.95	5.10	102	108 72		46	4
12	2730	965.2	0.98	4.80	102	111 75		46	4
13	3000	968.209	0.81	4.00	102	111 77		46	4
14	230	971.0	0.97	4.70	103	114 80		46	4
15	500	973.9	0.90	4.40	103	116 81		46	4
16	730	977.0	0.78	3.80	103	117 80		46	4
17	1000	979.6	0.74	3.60	103	120 83		46	5
18	1230	982.5	0.60	2.90	104	122 85		46	5
19	1500	984.8	0.71	3.45	103	121 86		46	3
20	1730	987.3	0.65	3.20	104	123 87		45	3
21	2000	989.9	0.72	3.50	104	124 88		45	3
22	2230	992.5	0.70	3.40	103	119 89		48	3
23	2500	995.0	0.72	3.50	103	126 89		48	3
24	2730	998.6	0.80	3.80	104	125 91		48	3
25	3000	000.498							

Leak check $\rightarrow 0.35 \rightarrow 0.05 = 0.000$ $\frac{11}{17}$
 pitot - $\rightarrow 4.0$
 pitot - $\rightarrow 4.4$
 63.017 8660 3.6804 101.63 99.81

Plant Louisiana Pacific - Merida MDF
 Sampling Location MDF Phase RTO Heat
 Test For HCOH / VOC
 Test Operators Russell McKnight

RUN No. 2
 Date 1-20-94
 Time start 1359 end 1500

Meter Box RAC 5913 49
 Sample Box No. 4
 Probe/Pitot 8' teflon
 Pitot Cp .84
 Nozzle Dia. .260
 Filter No.

No. Sample Pts. 12 x 2
 Minutes/Pt. 2.5
 NOMOGRAPH
 $\Delta H @$ 1.85
 Meter Temp.
 % H₂O
 C-Factor
 Stack Temp.
 Ref. ΔP .38

Gas Analysis AIR
 CO₂
 O₂
 CO
 Time

Condensate:
 tare Remarks fin
 Silica gel:
 tare fin

Remarks:
 1) DNPH 564.0 570.0
 2) DNPH 572.0 576.5
 3) AT 482.0 482.5
 4) S.G. 763.0 769.0

Amb. Temp. °F 47
 Bar. Press. "Hg
 Static Press. "H₂O ~~50~~ 2.6

16.5

Port Point	El. Time, Min.	DGM Reading, Ft.	Velocity Head ΔP , in. H ₂ O	Orifice ΔH in. H ₂ O	Stack Temp. °F	Meter Temp., °F In	Meter Temp., °F Out	Oven Temp. °F	Imp. Temp. °F	Vac in. Hg
1	000	000.995	0.76	3.70	96	78	76	N/A	44	7
2	230	004.0	0.81	4.00	96	79	76		48	5
3	500	007.0	0.81	4.00	97	87	76		48	5
4	730	009.1	0.82	4.00	98	88	76		48	5
5	1000	011.7	0.81	4.00	97	95	77		51	5
6	1230	015.0	0.75	3.60	97	99	78		50	5
7	1500	017.1	1.00	4.80	100	106	80		52	5
8	1730	020.1	1.35	6.60	98	107	80		50	5
9	2000	023.5	1.40	6.70	98	117	82		47	5
10	2230	027.0	1.40	6.70	97	117	82		46	5
11	2600	030.5	1.45	7.00	98	123	86		46	5
12	2730	034.3	1.45	7.00	97	125	84		46	5
13										
14	3010	038.028	1.25	6.60	100	126	90		47	6
15	230	041.7	1.25	6.60	98	125	91		46	6
16	500	044.8	1.20	6.40	98	128	91		46	6
17	730	048.5	1.15	5.50	98	130	95		47	6
18	1000	051.8	0.98	4.70	100	131	92		45	5
19	1230	054.8	0.87	4.30	97	131	93		46	5
20	1500	057.7	0.92	4.50	97	132	95		46	5
21	1730	060.9	0.90	4.40	98	134	95		46	5
22	2000	063.9	0.98	4.90	97	131	96		46	5
23	2230	067.3	0.93	4.80	96	132	96		47	5
24	2500	070.1	0.91	4.40	97	133	98		47	6
25	2730	072.9	0.91	4.40	97	134	98		47	6
26	3010	075.810								
27										
28										
29										
30										
31										
32										
33										
34										
35										

Leak Check: .031 → .031 = 0.000 up 10.46
 pitot + ve 6.0
 pitot - ve 5.0
 74.815
 5.1419
 99.58
 101.46
 .9922

Plant Louisiana Pacific - Womack MOF
 Sampling Location MOF 0 Press RTD Inlet
 Test For H₂OH/VOC
 Test Operators Russell/McKnight

RUN No. 3
 Date 1-20-94
 Time start 1559 end 1701

Meter Box RAC
 Sample Box Nm 4
 Probe/Pitot 8' Tefta
 Pitot Cp .848
 Nozzle Dia. .266
 Filter No. _____

No. Sample Pts. 12 x 2
 Minutes/Pt. 2.5

NOMOGRAPH
 $\Delta H @$ 1.85
 Meter Temp. _____
 % H₂O _____
 C-Factor _____
 Stack Temp. _____
 Ref. ΔP .38

Gas Analysis AIR
 CO₂ _____
 O₂ _____
 CO _____
 Time _____

Condensate:
 tare 2.5 fin _____
 Silica gel: _____
 tare _____ fin _____

Remarks:
ingingers Tars Final
1) DNPH 563.0 569.5
2) DNPH 570.5 571.0
3) MT 482.0 482.5
4) S.Gel 769.0 774.0

Amb. Temp. °F 45
 Bar. Press. "Hg _____
 Static Press. "H₂O -2.6

Port Point	El. Time, Min.	DGM Reading, Ft. ³	Velocity Head ΔP , in. H ₂ O	Orifice ΔH , in. H ₂ O	Stack Temp. °F	Meter Temp., °F In Out	Oven Temp. °F	Imp. Temp. °F	Vac in. Hg
1	1200	076.114	0.52	2.45	89	75 75	119	44	3
2	230	078.7	0.63	2.00	92	79 76		45	3
3	500	080.7	0.63	3.00	94	83 77		43	3
4	730	082.9	0.60	2.90	94	83 78		44	3
5	1000	085.1	0.61	3.00	97	89 78		44	3
6	1230	087.4	0.55	2.70	95	96 77		44	3
7	1500	089.7	0.72	3.50	96	100 79		45	3
8	1730	092.5	0.94	4.60	100	103 78		45	3
9	2000	095.9	0.97	4.70	100	108 80		45	3
10	2230	098.2	0.94	4.60	98	111 79		45	3
11	2500	101.7	0.91	4.50	98	116 83		45	3
12	2730	104.6	0.88	4.30	98	120 83		45	3
1	3000	107.164	0.83	4.10	97	119 83		45	3
2	230	110.2	0.90	4.60	99	119 84		45	3
3	500	113.4	0.93	4.70	99	120 83		45	3
4	730	116.5	0.74	3.65	100	122 88		45	3
5	7000	119.3	0.70	3.40	99	124 89		45	3
6	1230	121.7	0.58	2.80	100	125 91		45	3
7	1500	124.3	0.65	3.10	100	125 91		45	3
8	1730	127.0	0.71	3.45	102	123 91		44	3
9	2000	129.0	0.72	3.45	101	124 91		45	3
10	2230	131.6	0.72	3.45	100	124 92		45	3
11	2500	134.3	0.66	3.20	100	126 94		46	3
12	2730	136.8	0.67	3.25	100	126 94		45	3
and	60	139.066							

Leak check: .068 → 070 = .002 per 9" Hg
 pitot at 5.6
 pitot at 3.1

62.952 4554 3.6000 97.88 96.96

APPENDIX B.

RECORDER TRACES/DATA LOG

Louisiana Pacific Corporation - Urania MDF Plant
MDF Dryers - RTO North Outlet and RTO Inlet
NOx/CO CEM Data Acquisition - 10 Minute Data Log

Run 1									
Log Time		Ch 1 Volts	NOx ppm Outlet	Ch 2 Volts	CO ppm Outlet	Ch 3 Volts	NOx ppm Inlet	Ch 4 volts	CO ppm Inlet
1108	1118	12.5	31.3	1.0	5.0	7.9	19.8	1.2	12.0
1118	1128	12.2	30.5	1.1	5.5	7.5	18.8	1.0	10.0
1128	1138	12.2	30.5	0.9	4.5	7.9	19.8	1.2	12.0
1138	1148	12.5	31.3	1.1	5.5	8.1	20.3	1.1	11.0
1148	1158	12.2	30.5	1.1	5.5	8.1	20.3	1.2	12.0
1158	1208	12.1	30.3	0.9	4.5	8.1	20.3	1.1	11.0
AVERAGES:			30.7		5.1		19.8		11.3

Run 2									
Log Time		Ch 1 Volts	NOx ppm Outlet	Ch 2 Volts	CO ppm Outlet	Ch 3 Volts	NOx ppm Inlet	Ch 4 volts	CO ppm Inlet
1459	1509	12.0	30.0	0.8	4.0	8.8	22.0	1.0	10.0
1509	1519	11.3	28.3	0.7	3.5	8.2	20.5	1.1	11.0
1519	1529	11.8	29.5	0.7	3.5	8.1	20.3	1.6	16.0
1529	1539	11.5	28.8	0.8	4.0	7.6	19.0	1.8	18.0
1539	1549	11.0	27.5	0.7	3.5	7.8	19.5	1.8	18.0
1549	1559	10.9	27.3	0.7	3.5	5.5	13.8	1.7	17.0
AVERAGES:			28.5		3.7		19.2		15.0

Run 3									
Log Time		Ch 1 Volts	NOx ppm Outlet	Ch 2 Volts	CO ppm Outlet	Ch 3 Volts	NOx ppm Inlet	Ch 4 volts	CO ppm Inlet
1656	1706	6.8	17.0	0.4	2.0	2.2	5.5	1.0	10.0
1706	1716	7.9	19.8	0.3	1.5	9.0	22.5	2.2	22.0
1716	1726	9.2	23.0	0.2	1.0	17.0	42.5	1.1	11.0
1726	1736	9.9	24.8	0.3	1.5	17.5	43.8	1.0	10.0
1736	1746	10.4	26.0	0.2	1.0	15.5	38.8	1.0	10.0
1746	1756	10.2	25.5	0.2	1.0	12.8	32.0	1.2	12.0
AVERAGES:			22.7		1.3		30.8		12.5

Louisiana Pacific Corporation - Uriaia MDF Plant
MDF Press Vent Rto Inlet/Outlet Test 1-21-94
NOx/CO CEM Data Acquisition - 10 Minute Data Log

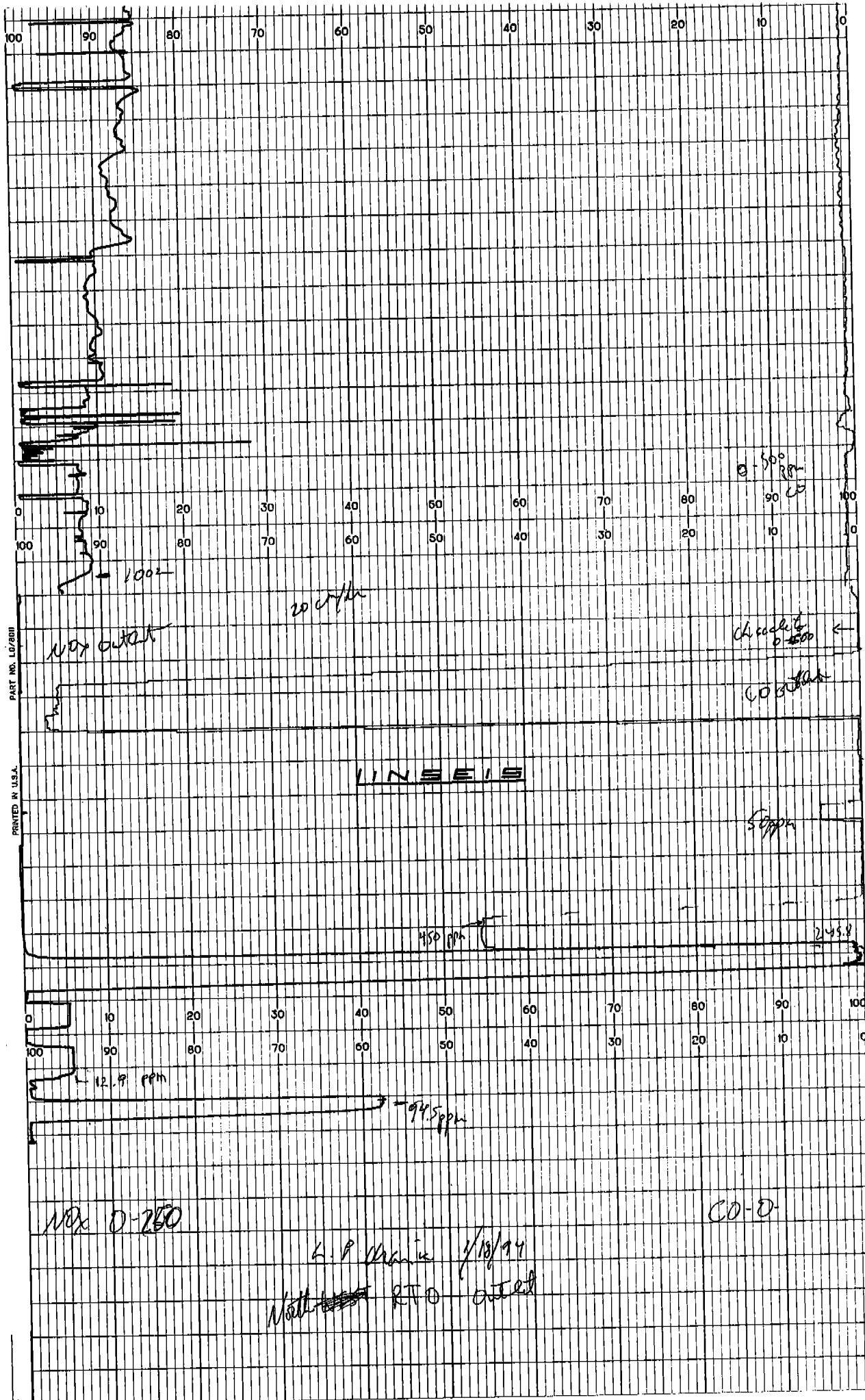
Run 1									
Log Time		Ch 1 Volts	NOx ppm Outlet	Ch 2 Volts	CO ppm Outlet	Ch 3 Volts	NOx ppm Inlet	Ch 4 volts	CO ppm Inlet
0816	0826	8.9	8.9	1.5	3.0	0.0	0.0	0.0	0.0
0826	0836	9.1	9.1	1.6	3.2	0.0	0.0	0.0	0.0
0836	0846	9.0	9.0	1.5	3.0	0.0	0.0	0.0	0.0
0846	0856	9.6	9.6	1.6	3.2	0.0	0.0	0.0	0.0
0856	0906	9.8	9.8	1.7	3.4	0.0	0.0	0.0	0.0
0906	0916	9.8	9.8	1.5	3.0	0.0	0.0	0.0	0.0
AVERAGES:			9.4		3.1		0.0		0.0

Run 2									
Log Time		Ch 1 Volts	NOx ppm Outlet	Ch 2 Volts	CO ppm Outlet	Ch 3 Volts	NOx ppm Inlet	Ch 4 volts	CO ppm Inlet
1001	1012	8.7	8.7	1.1	2.2	0.0	0.0	0.0	0.0
1012	1022	7.7	7.7	0.9	1.8	0.0	0.0	0.0	0.0
1022	1032	7.9	7.9	1.0	2.0	0.0	0.0	0.0	0.0
1032	1042	8.2	8.2	1.0	2.0	0.0	0.0	0.0	0.0
1042	1052	8.5	8.5	0.9	1.8	0.0	0.0	0.0	0.0
1052	1102	8.6	8.6	1.0	2.0	0.0	0.0	0.0	0.0
AVERAGES:			8.3		2.0		0.0		0.0

Run 3									
Log Time		Ch 1 Volts	NOx ppm Outlet	Ch 2 Volts	CO ppm Outlet	Ch 3 Volts	NOx ppm Inlet	Ch 4 volts	CO ppm Inlet
1226	1236	8.4	8.4	1.3	2.6	0.0	0.0	0.0	0.0
1236	1246	8.7	8.7	1.1	2.2	0.0	0.0	0.0	0.0
1246	1256	9.0	9.0	0.9	1.8	0.0	0.0	0.0	0.0
1256	1306	8.9	8.9	1.0	2.0	0.0	0.0	0.0	0.0
1306	1316	8.8	8.8	1.1	2.2	0.0	0.0	0.0	0.0
1316	1326	8.9	8.9	1.0	2.0	0.0	0.0	0.0	0.0
AVERAGES:			8.8		2.1		0.0		0.0

MDF DRYERS NORTH RTO

CO/NOX TRACES



PRINTED IN U.S.A.

LINE 15

50 pp

450 pp
API

0 10 20 30 40 50 60 70 80 90 100
100 90 80 70 60 50 40 30 20 10 0

END RICE 1217
1215

no data

1200

no data

1200

5.1

1145

0 10 20 30 40 50 60 70 80 90 100
100 90 80 70 60 50 40 30 20 10 0

1130

MDF DRYERS NORTH RTO
NOx AND CO TRACES
RUN 1 (1108-1208)
1/18/94

1115

1112

LINE 15

START RICE 1108

1105

North Outer

The creek

0 10 20 30 40 50 60 70 80 90 100
100 90 80 70 60 50 40 30 20 10 0

PART NO. LO/BOI

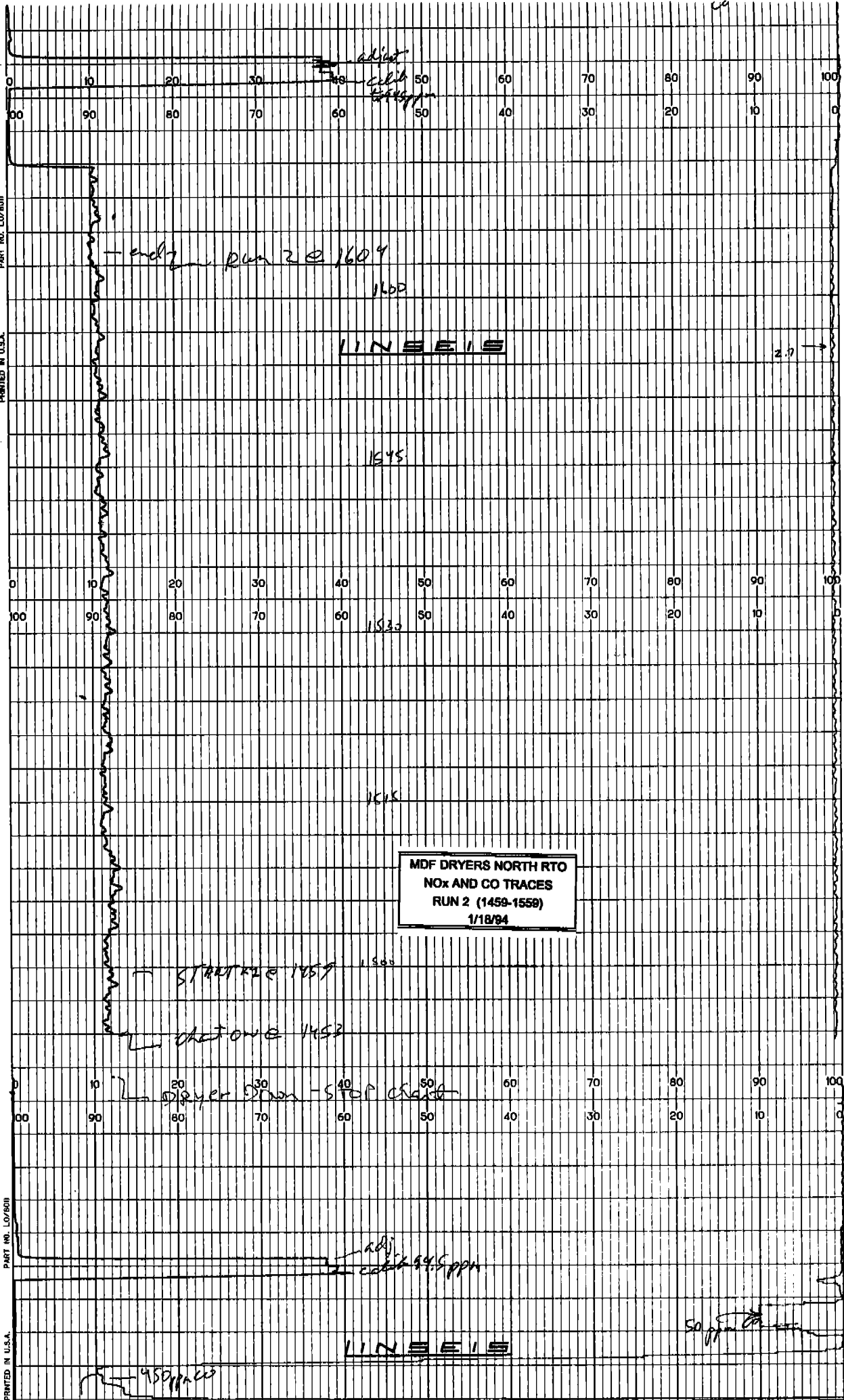
PRINTED IN U.S.A.

PART NO. LO/BOH

PRINTED IN U.S.A.

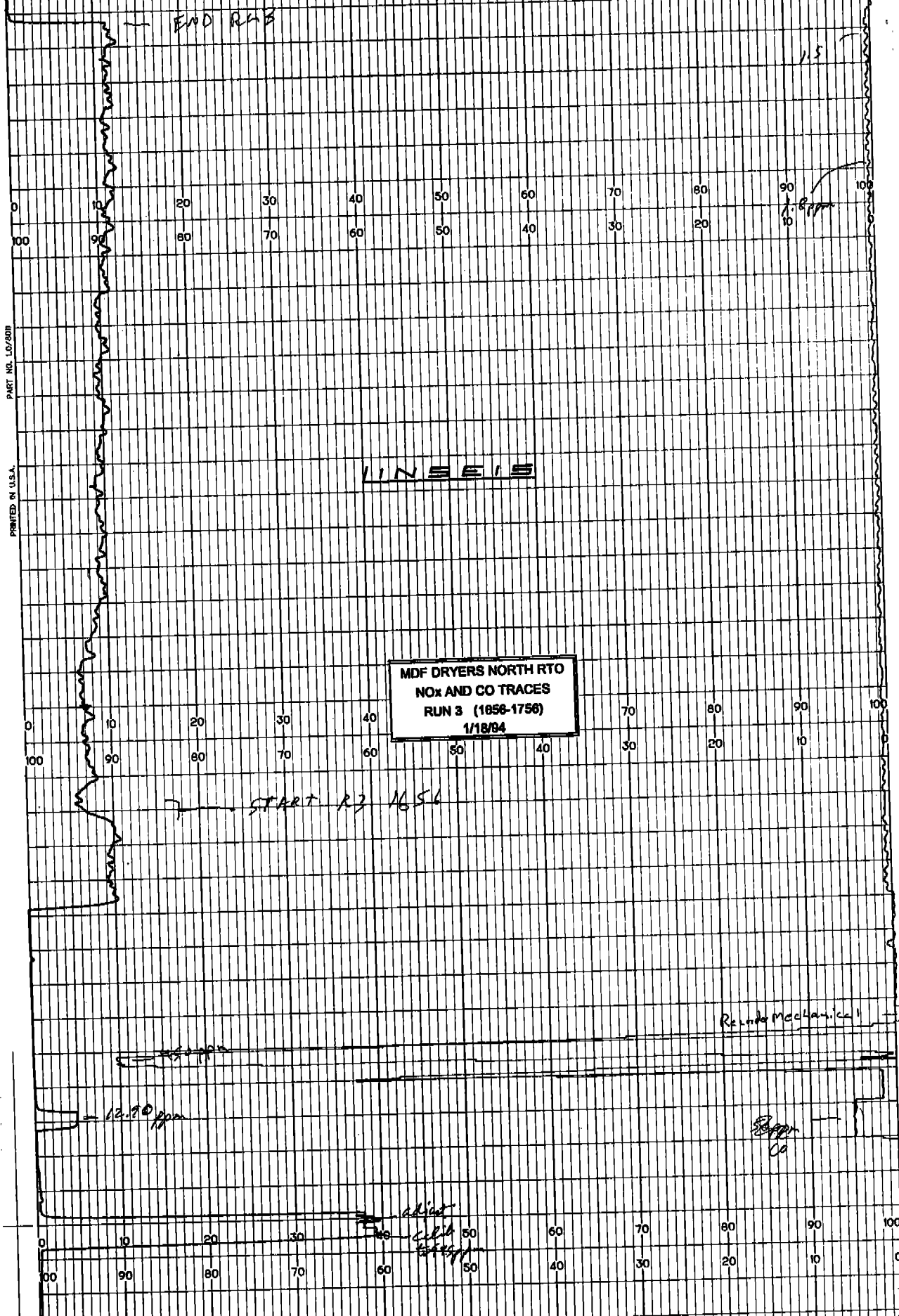
PART NO. LO/BOH

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PART NO. 1.0/2011

PRINTED IN U.S.A.



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Zero

LINSEIS

25.2

92.21 p.m

END RLB

45

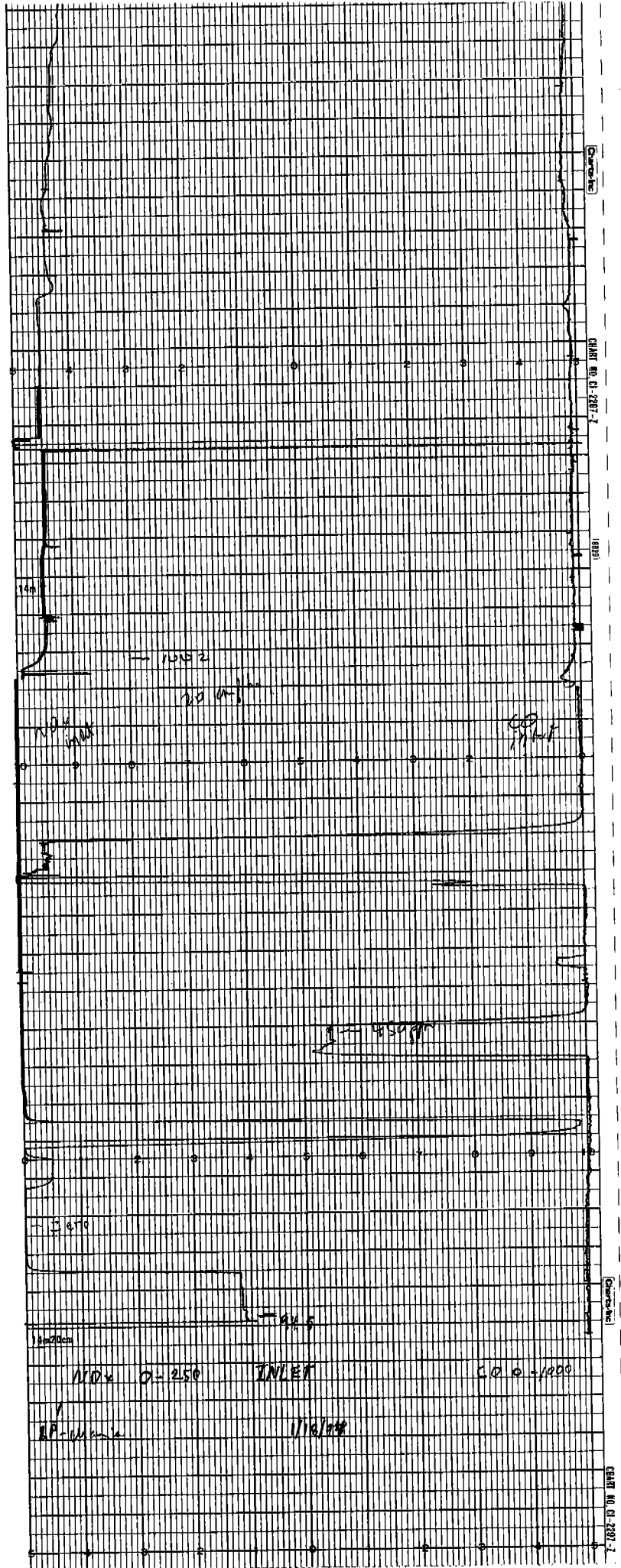
90
1.8 ppm
10

LINSEIS

**MDF DRYERS NORTH RTO
NOx AND CO TRACES
RUN 3 (1658-1756)
1/18/94**

MDF DRYERS RTO INLET

CO/NOX TRACES



6.95 6.95

EMPIR 5 12.7

1.96500

Time 12:00:00
Date 1/18/94

MDF DRYERS RTO INLET
NOx AND CO TRACES
RUN 1 (1108-1208)
1/18/94

NOx
2.0
1.0
0.0

CO
2.0
1.0
0.0

START TIME 11:57
4.600 100% - 100%

1/18/94

MDF Dryers

END RET 1609 1102

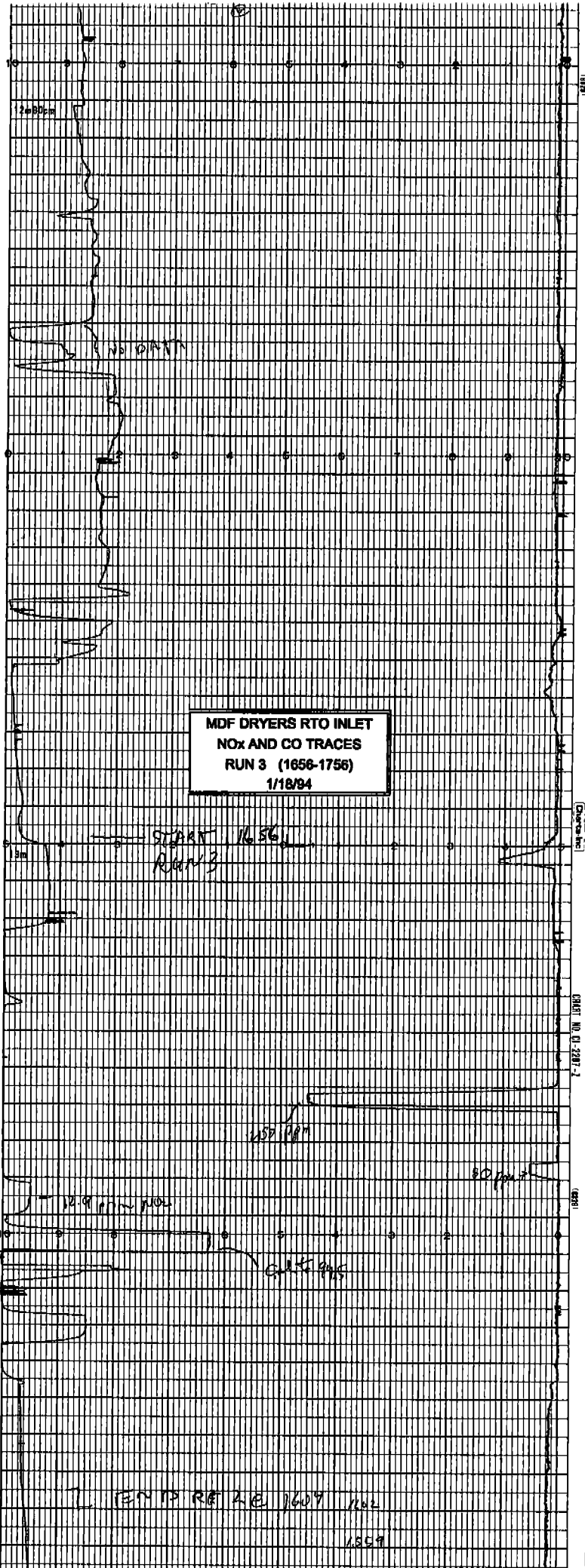
1559

19m20m

MDF DRYERS RTO INLET
NOx AND CO TRACES
RUN 2 (1459-1558)
1/18/94

Start one 1459 START
to 1459 DOWN
5-55 CHART

1459 1455



2000cm

Check of End Day 1-18-94

Zero

4.50

4.50

2.9 ppm NOx

Not a good start
End Day

2000cm

NO DATA

MDF DRYERS RTO INLET
NOx AND CO TRACES
RUN 3 (1658-1756)
1/18/94

START 1656
Run 3

Chart No. 3-2297-1

Chart No. 3-2297-1

Chart No. 3-2297-1

Chart No. 3-2297-1

MDF DRYERS
NORTH RTO AND RTO INLET

VOC TRACES

**MDF DRYERS
NORTH RTO INLET
AND RTO INLET
VOC TRACES
RUN 1 (1108-1511)
1/18/84**

QW-LET

11/98 5-ent-80/R

-(Ch to 0-100 on recorder)

INLET

START P/C
1105

PRINTED IN U.S.A.

937 SYSCAL

5 yr old 82.2

INSEIS

V - Sys Col 922

SysCAD to 937 / 937

SysCat
92.2

54502 486

Sys Cal 406

inst. cal 486 ppm

486 ppm INST. ADJUST

$$= \frac{406}{100} \text{ unit object}$$

at outlet $\Delta \sim 1000$ ppm

of the Right

 $R \neq L$

1902 ET 90

End 1516

59

75

62

77

82

74

82

81

74

MDF PRO
INLET 65

NORTH MDF RTO

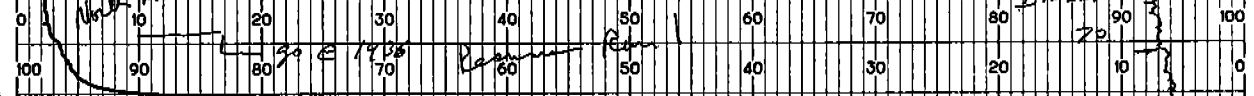


chart off 1327 one 1127

PART NO. LD/8011
PRINTED IN U.S.A.

chart off 1224 one 1301

LINE IS

sys cell 92.1

R. 1300
system cell 6



check out 2000

make out
done 1126

MDF DRYERS
NORTH RTO INLET
AND RTO INLET
VOC TRACES
RUN 1 (1108-1511)
1/19/94

Ben 1130

58

66

64

72

68

77

55

49

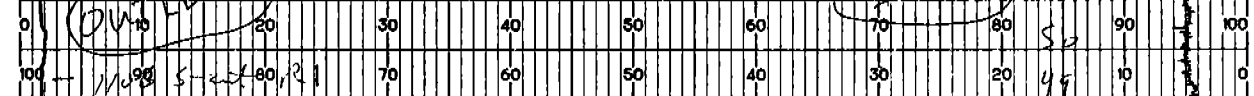
52

0-100 ppm

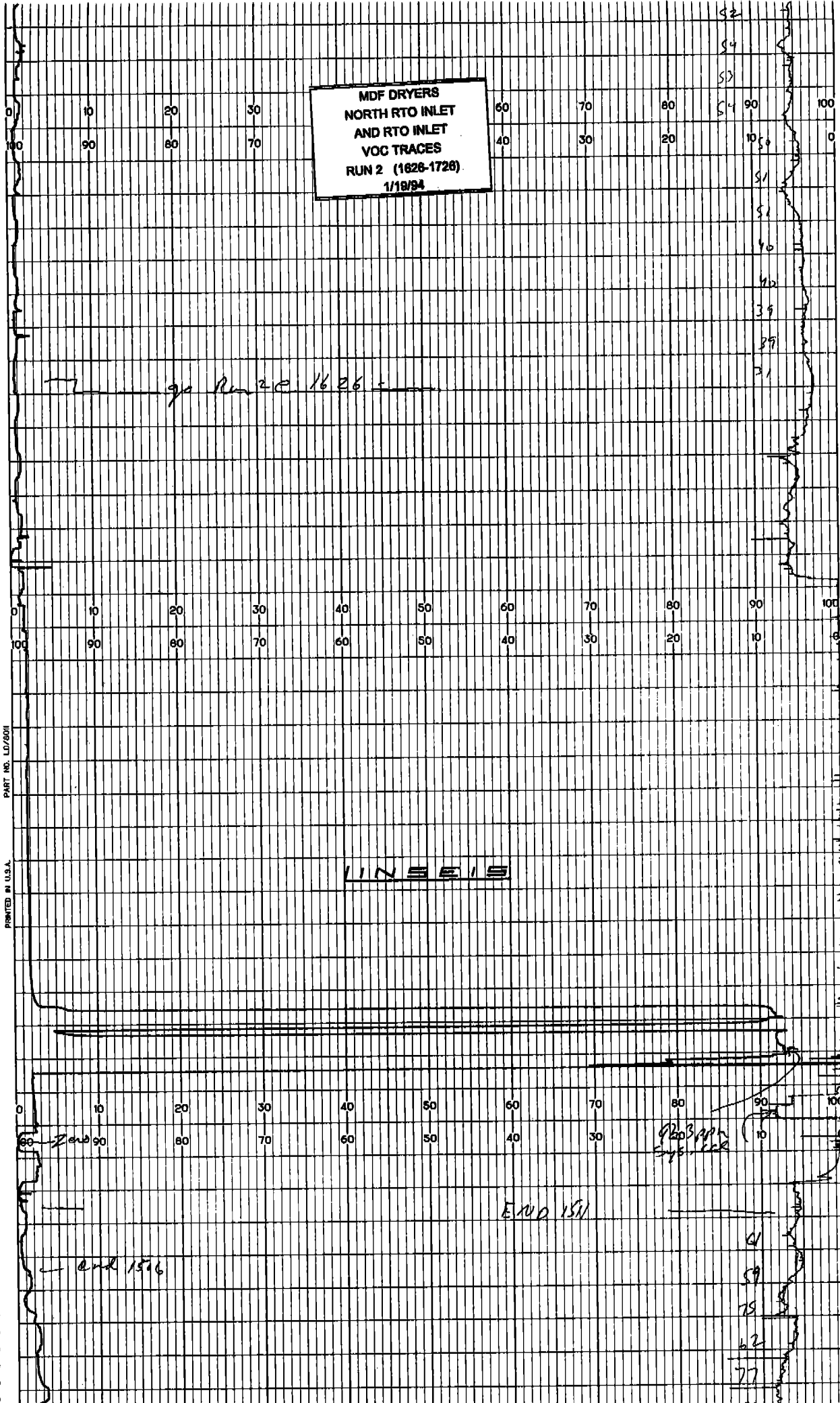
OUTLET

1000

INLET

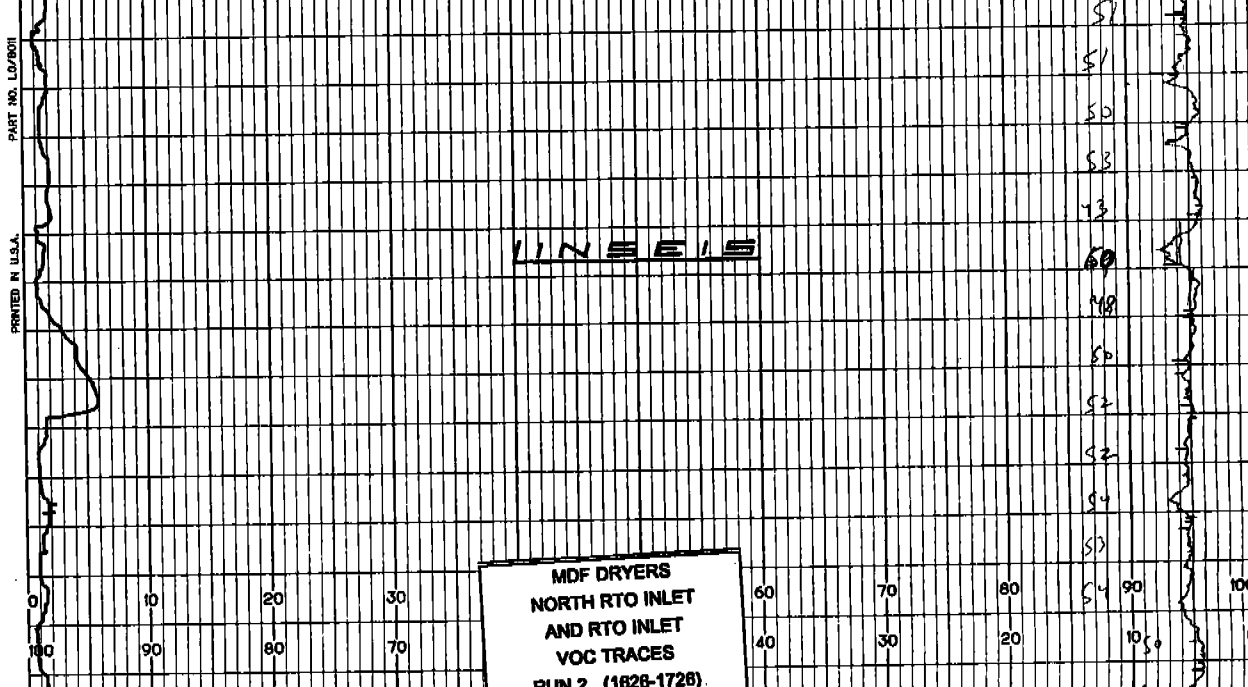
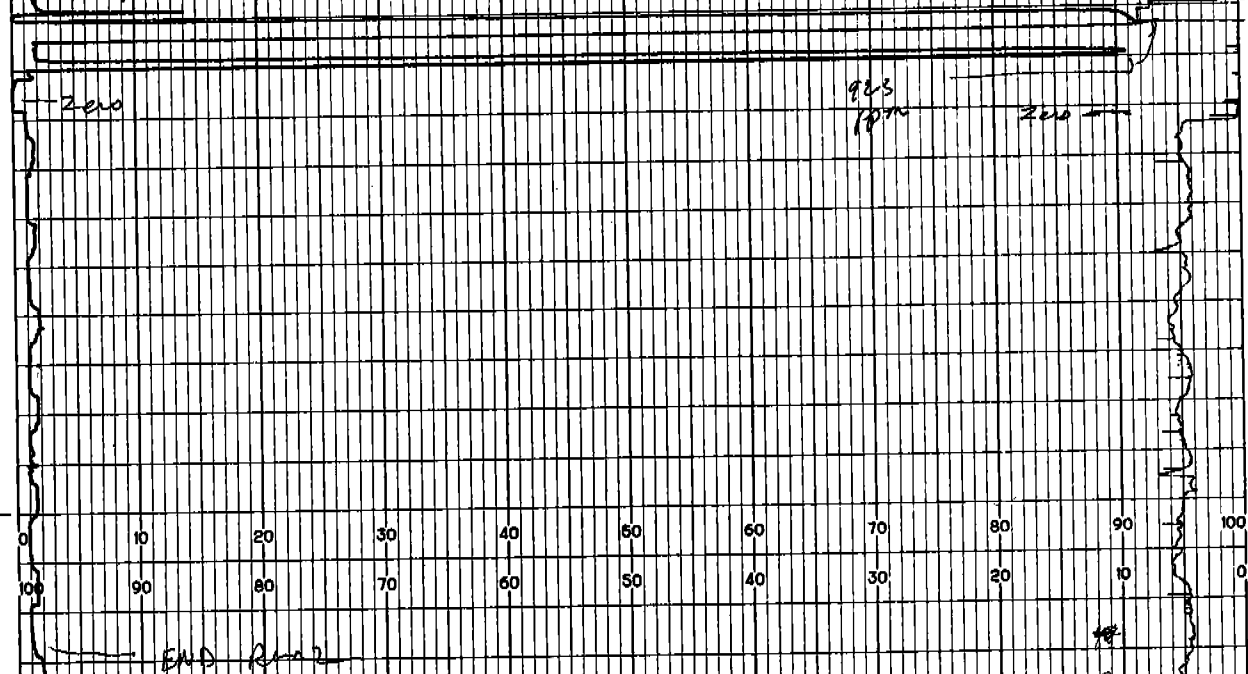
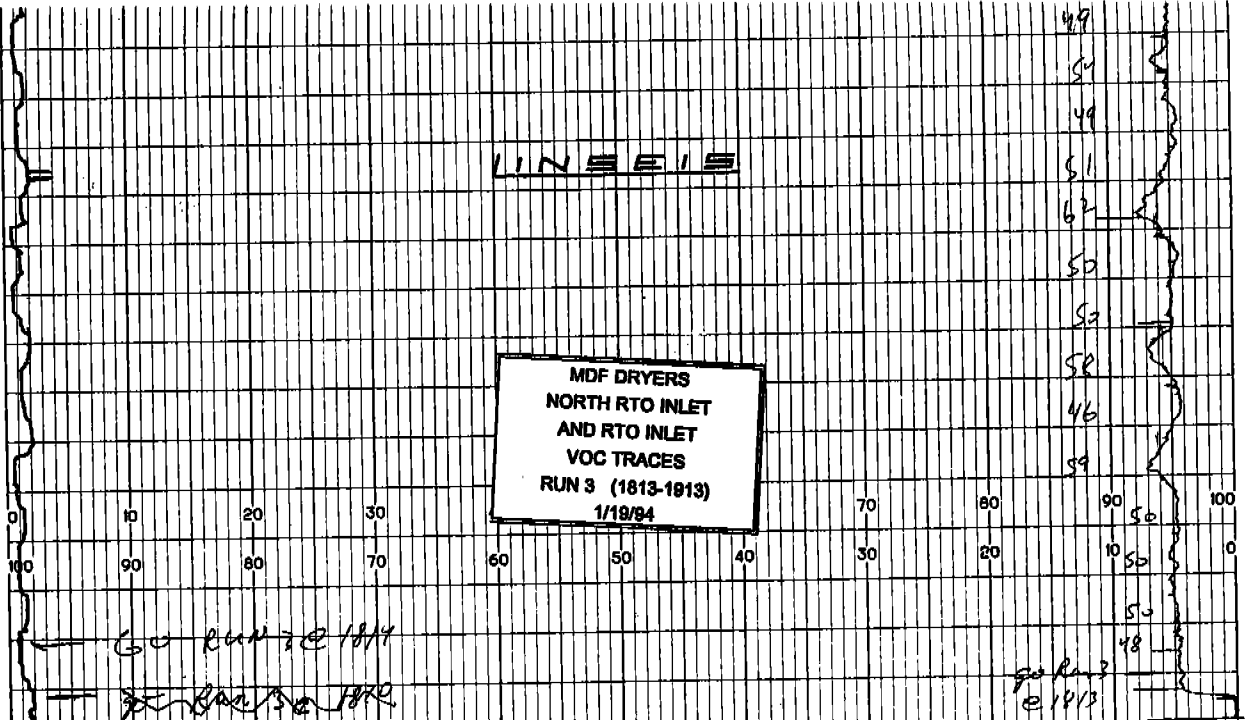


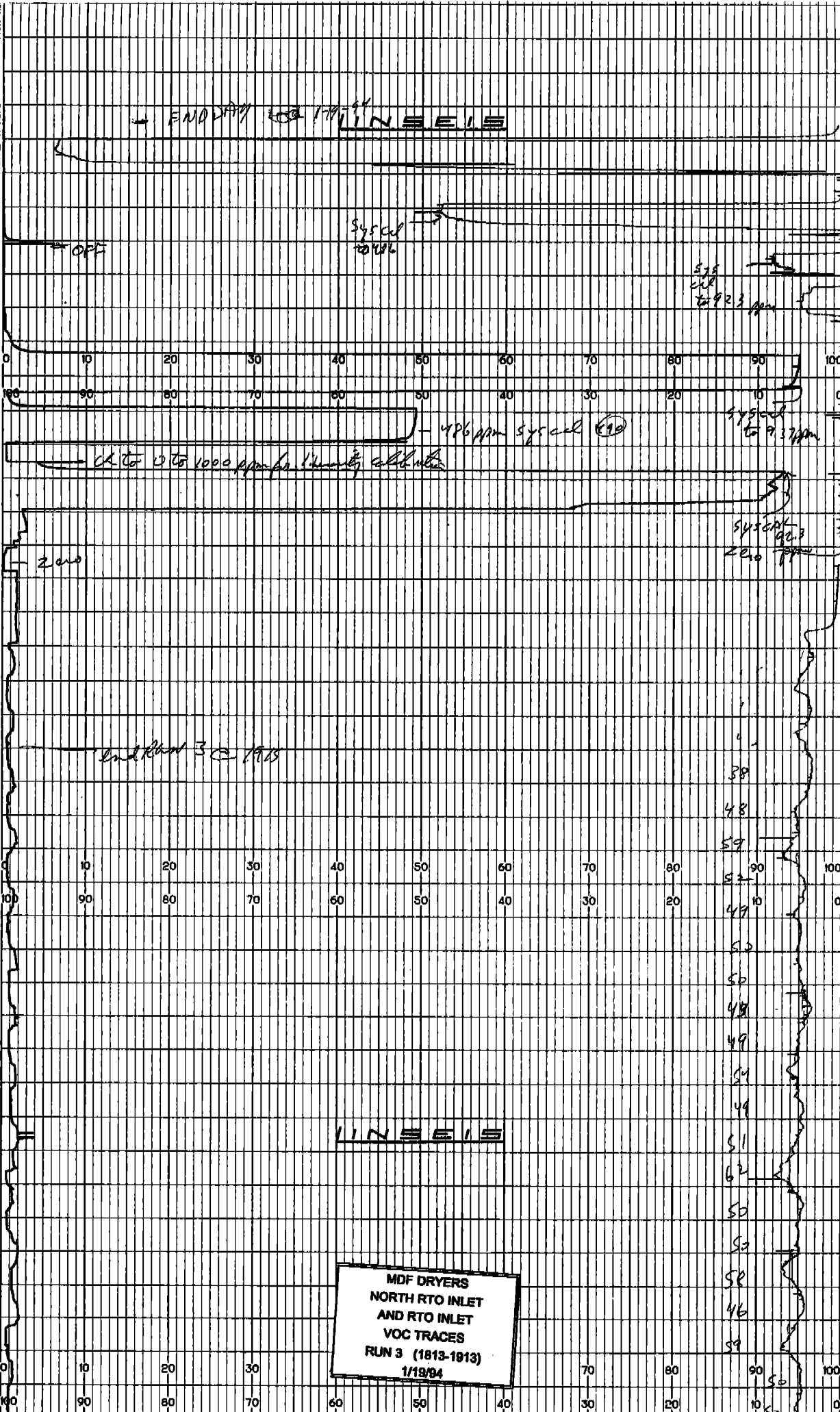
MDF DRYERS
NORTH RTO INLET
AND RTO INLET
VOC TRACES
RUN 2 (1626-1726)
1/19/94



PART NO. LD/501

PRINTED IN U.S.A.





PRESS VENT RTO

CO/NO_x TRACES

PART NO. LO/6001

PRINTED IN U.S.A.

INSEIS

PRESS VENT RTO
NOx AND CO TRACES
RUN 1 (0816-0916)
1/21/84

Stat R1 0816
ch 6 0-100
Outlet NOx TECO 125 ppm

Outlet
CO 0-200
TECO 48H

ch 6 0-200
0-200 ppm

12.91 ppm NOx
ch 6 0-100
12.91 ppm NOx
ch 6 0-100

12.91 ppm NOx
ch 6 0-100
12.91 ppm NOx
ch 6 0-100

12.91 ppm NOx
ch 6 0-100
12.91 ppm NOx
ch 6 0-100

PART NO. LO/6001

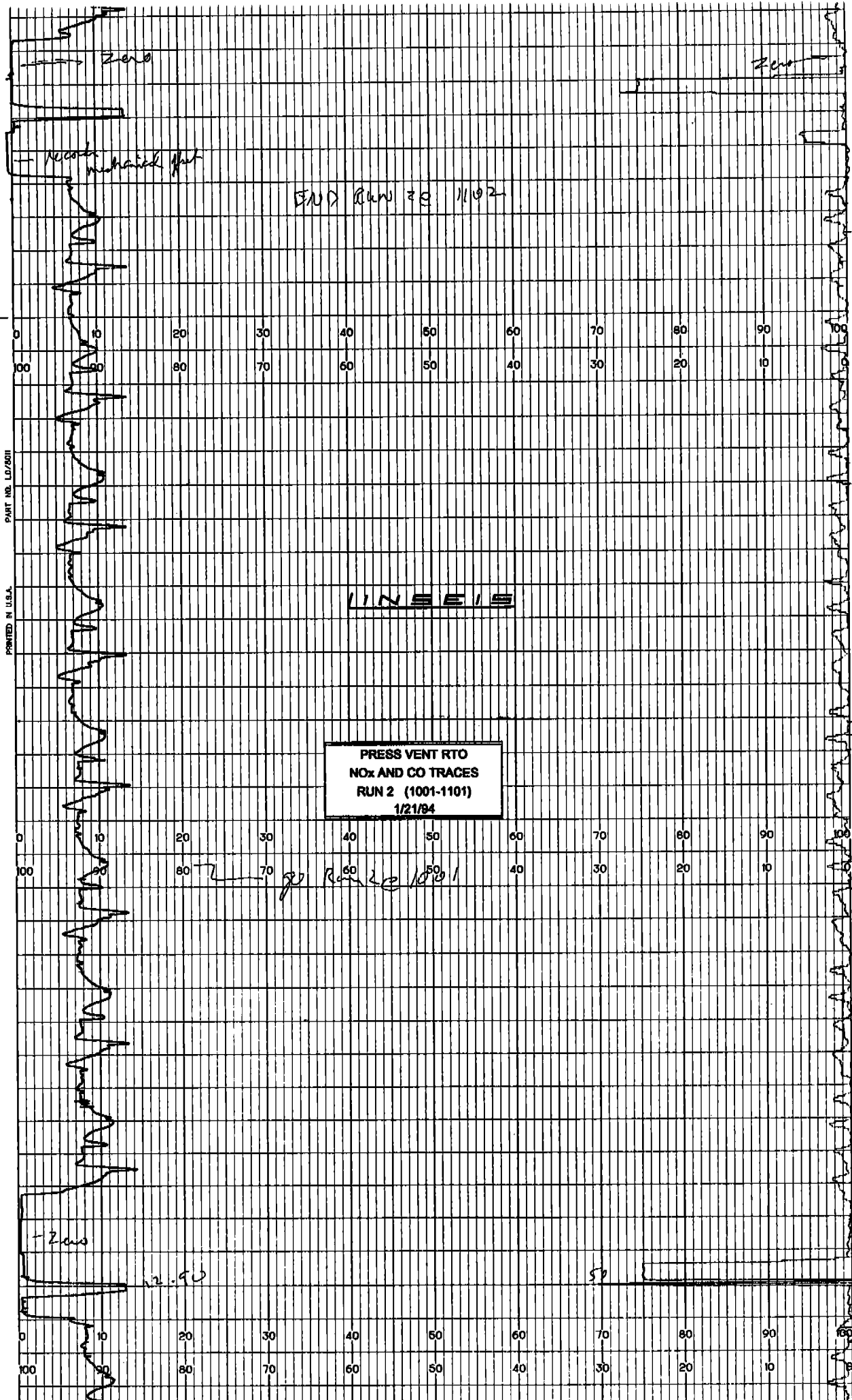
PRINTED IN U.S.A.

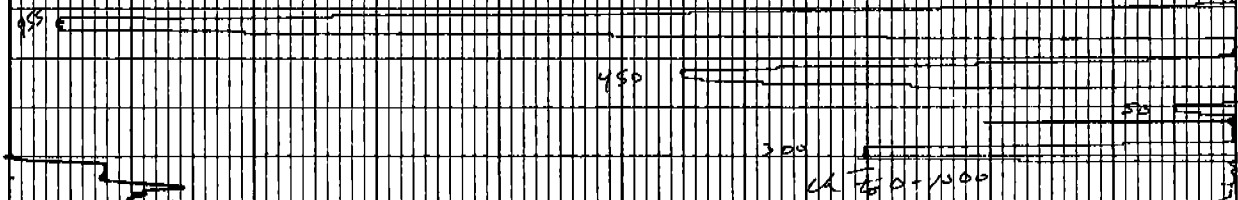
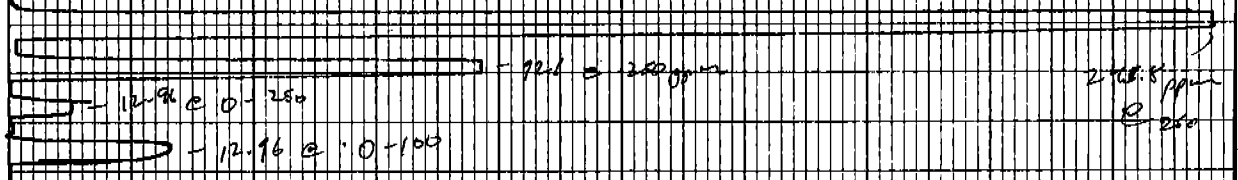
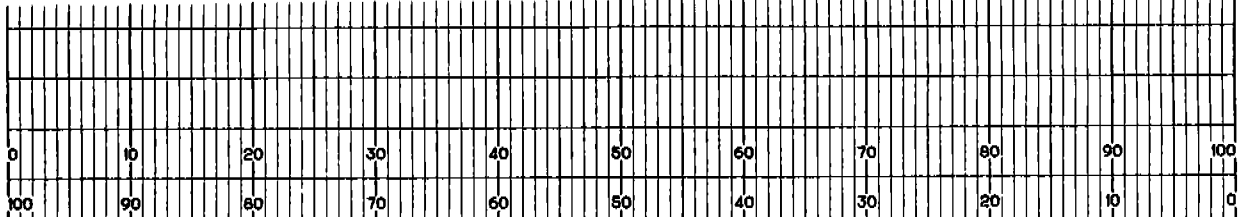
INSEIS

0716

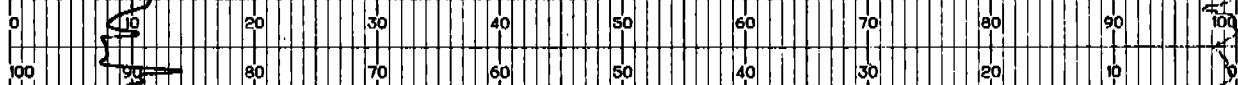
0716

PART NO. LD/5011
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END R3 1327

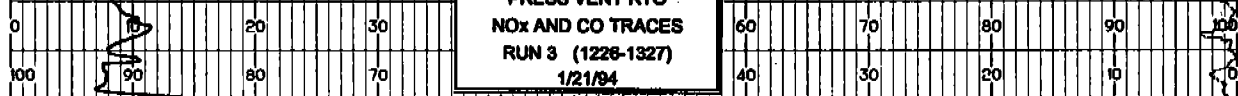


PART NO. LO/801

PRINTED IN U.S.A.

UNSELS

PRESS VENT RTO
NOx AND CO TRACES
RUN 3 (1226-1327)
1/21/94



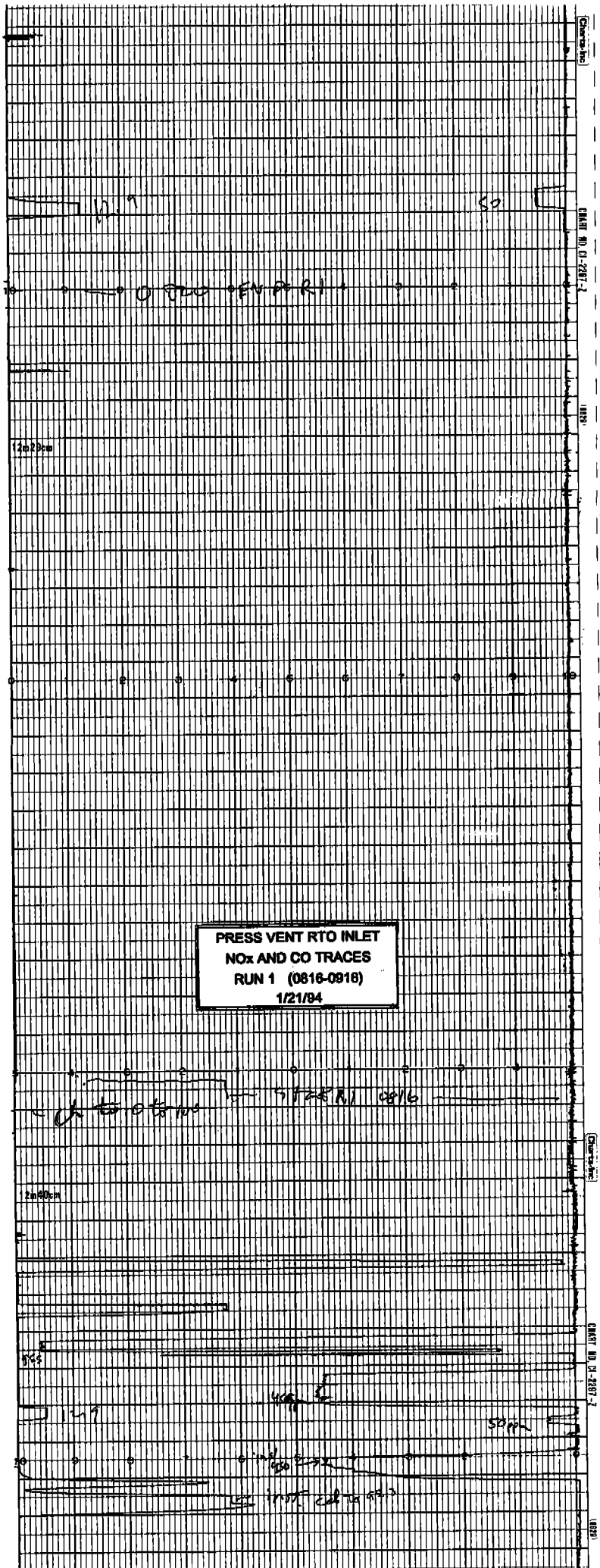
7 30 R-2 @ 1226

Zero

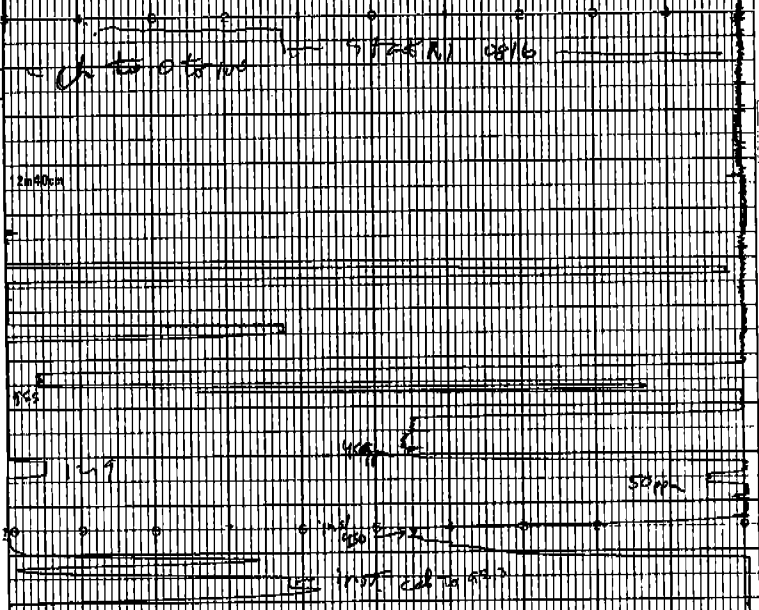
Zero

PRESS VENT RTO INLET

CO/NOX TRACES



PRESS VENT RTO INLET
NOx AND CO TRACES
RUN 1 (0816-0918)
1/21/94



PRESS VENT RTO INLET
NOx AND CO TRACES
RUN 3 (1226-1327)
1/21/94

96 K30 1225

10000

END RUN 3

PRESS VENT RTO INLET
NOx AND CO TRACES
RUN 2 (1001-1101)
1/21/94

60 RUN 2 1100

END DAY 1-21-94

9:55 PM

9:50 PM

5:00 PM

2:55 PM

9/6

9:50 PM

13.96 PM = 9-100 PM 5:45 PM

END 12:26

10:00 PM

PRESS VENT RTO INLET
NOx AND CO TRACES
RUN 3 (1226-1327)
1/21/94

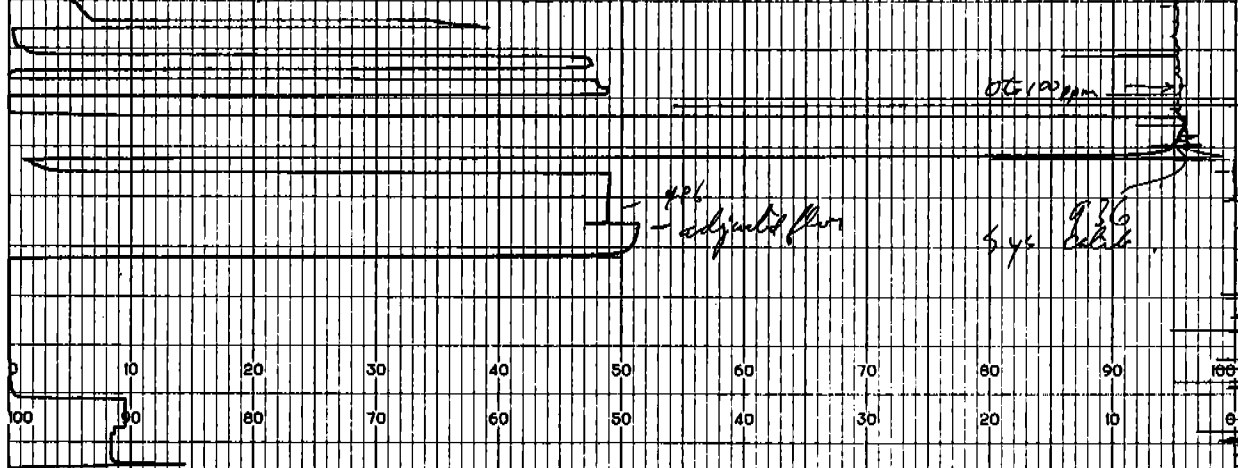
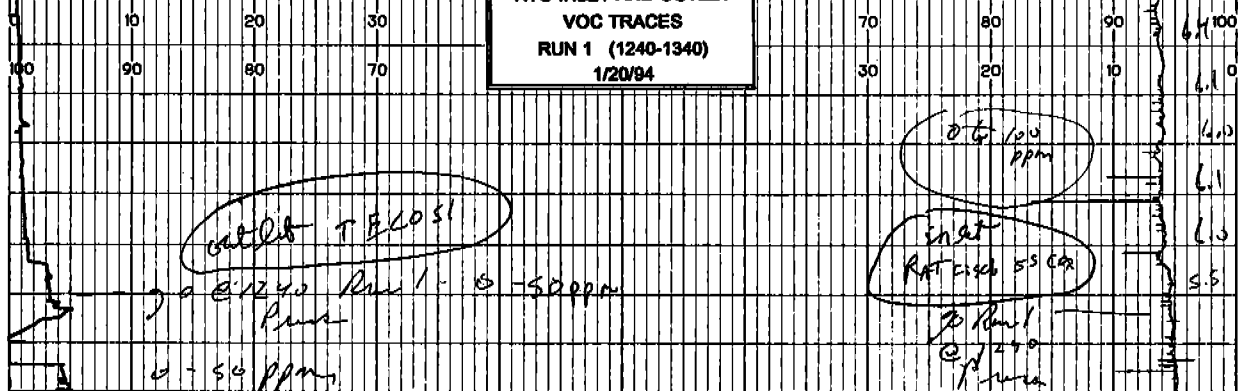
90 KBA 1225

PRESS VENT RTO
AND RTO INLET

VOC TRACES

L I N E S E I S

PRESS VENT
RTO INLET AND OUTLET
VOC TRACES
RUN 1 (1240-1340)
1/20/94



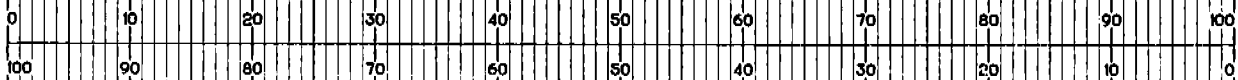
OUTLET

INLET

92.3 ppm 0-100 ppm Sys F I N S E I S

Pure Vent outlet + heat VOC
1-20-94

92.3 ppm
0-100 ppm



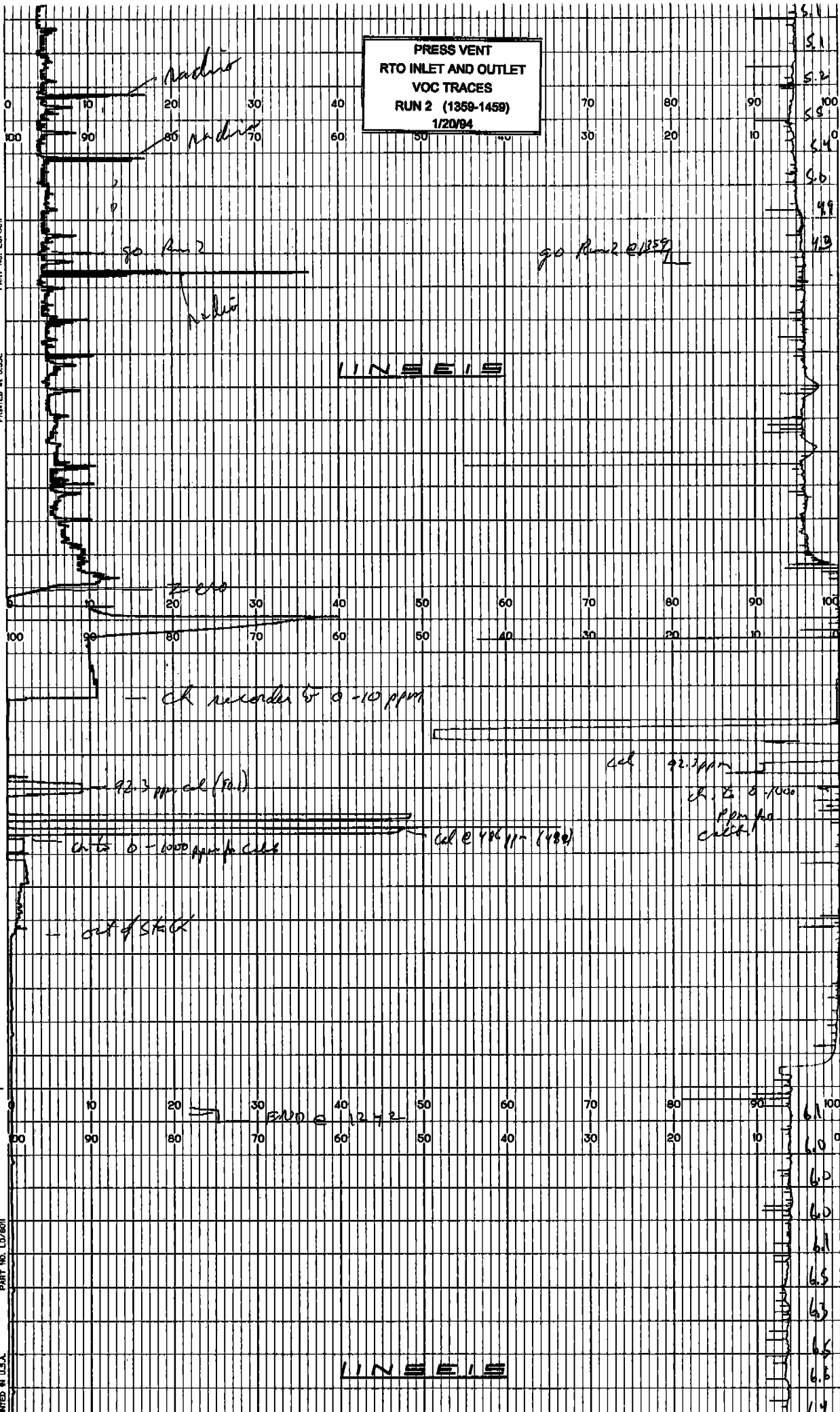
PRESS VENT
RTO INLET AND OUTLET
VOC TRACES
RUN 2 (1359-1459)
1/20/94

PART NO. LD/801

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PART NO. LD/801

PRINTED IN U.S.A.



PRESS VENT
RTO INLET AND OUTLET
VOC TRACES
RUN 3 (1600-1700)
1/20/84

start R3 @ 1600

stat R3 @ 1559

6.80

6.9
6.8
6.3
6.1
5.9

PART NO. LD/8011

PRINTED IN U.S.A.

INSEIS

check of
149
CH2

END RUN 2 @ 1500

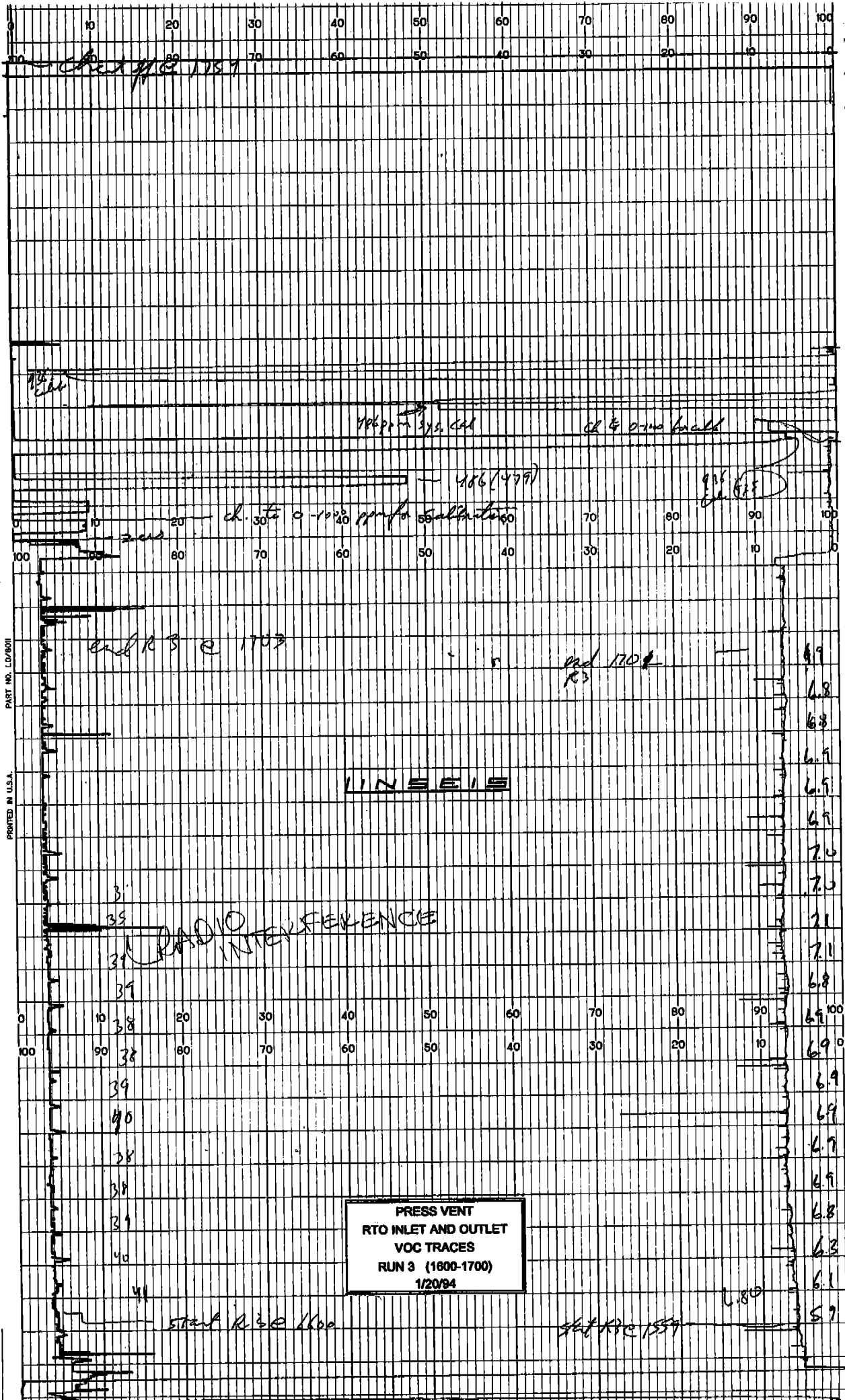
out

4.8
4.8
4.8
4.9
4.9
5.0
5.0
5.0
5.0
5.0
5.1
5.1
5.2
5.3
5.4

PRESS VENT
RTO INLET AND OUTLET
VOC TRACES
RUN 2 (1359-1459)
1/20/84

radio

radio



4.9
6.8
6.8
6.9
6.9
6.9
7.0
7.0
7.1
7.1
6.8
6.9
6.9
6.9
6.9
6.8
6.3
6.1
5.9

3
35
31
39
38
38
39
40
38
38
39
40
41

start R3 @ 1600

end R3 @ 1759

6.80

APPENDIX C.

CALIBRATION DATA

DRY GAS METER CALIBRATION

Meter ID Andersen
 Calibration Method DGM/DGM By DGR
 Calibration Meter ID 651729 Pbar 29.95
 Date 11/22/93

Vcal in Hg	DP in.	Time min	Calibrating Meter			Field Meter						Y	Q	K	DH@
			V1 cf	V2 cf	Temp F	V1 cf	V2 cf	Temp. in		Temp. out					
								init	final	init	final				
1	5.00	8.33	887.293	897.494	69	574.007	584.124	68	90	68	70	1.005	1.21	0.7	1.8932
1	4.00	9.50	897.494	907.956	69	584.124	594.686	87	108	70	77	1.011	1.1	0.71	1.8525
1	3.00	10.00	907.956	917.643	72	594.686	604.589	106	118	78	87	1.017	0.98	0.72	1.7816
1	2.00	12.50	917.643	927.274	69	604.589	614.675	110	118	88	96	1.011	0.8	0.71	1.82
1	1.00	16.50	927.274	936.795	70	614.675	624.8	112	118	95	102	1.003	0.61	0.76	1.6057
Averages:												1.011			1.7906

$$Y = [V_{cal}](P_{bar})(T_{dgm}) / [(V_{dgm})(P_m)(T_{cal})]$$

$$K = Q(\sqrt{(P_m M_m)}) / ((T_{m, out})(DH))$$

$$Q = ((V_{mi} - V_{mf}) / \text{min.})(T_{M, out} / T_{m, avg})(Y)$$

$$DH@ = 0.921 / K^2$$

Where:

Y = Meter correction factor, dimensionless

Vcal = Volume of gas through calibrating meter, cubic feet

Vdgm = Volume of gas through field dry gas meter, cubic feet

Pbar = Barometric pressure, in. Hg

Pm = Meter pressure, (Pbar = DH/13.6)

Tdgm = Average dry gas meter temp, degrees R

Tcal = Temperature of gas at calibrating meter, degrees R

DRY GAS METER CALIBRATION

Meter ID RAC
Calibration Method DGM/DGM **By** BMCK
Calibration Meter ID 651729 **Pbar** 29.87
Date 1/23/94

Vac. in. Hg	DH in. H2O	Time min	Calibrating Meter			Field Meter						Y	Q	K	DH@
			Vi cf	Vf cf	Temp F	Vi cf	Vf cf	Temp. in		Temp out					
								init.	final	init.	final				
1	2.70	66.00	96.412	154.944	68	274.546	334.993	68	129	68	91	1.000	0.9	0.7	1.899
1	2.70	20.15	154.944	172.577	67	334.993	354.062	125	132	92	97	0.996	0.91	0.7	1.890
1	2.70	22.00	172.577	191.882	67	354.062	374.883	128	135	98	100	1.005	0.92	0.7	1.865
Averages:												1.00			1.88

$$Y = [Vcal](Pbar)(Tdgm)/[(Vdgm)(Pm)(Tcal)]$$

$$K = Q(\sqrt{(Pm \text{ Mm})/(Tm \text{ out})(DH)})$$

$$Q = ((Vmi-Vmf)/min.)(TM,out/Tm,avg)(Y)$$

$$DH@ = 0.921/K^2$$

Where:

Y = Meter correction factor, dimensionless

Vcal = Volume of gas through calibrating meter, cubic feet

Vdgm = Volume of gas through field dry gas meter, cubic feet

Pbar = Barometric pressure, in. Hg

Pm = Meter pressure, (Pbar = DH/13.6)

Tdgm = Average dry gas meter temp, degrees R

Tcal = Temperature of gas at calibrating meter, degrees R

APPENDIX D.

**FORMALDEHYDE ANALYSIS
(AIR TECHNIQUES/OXFORD LABORATORIES)**

APPENDIX E.

(ARMSTRONG ENVIRONMENTAL REPORT)

Compliance Emissions Sampling
Louisiana Pacific
Urania, LA
January 18-19, 1994
Armstrong Environmental Inc.
Project W-1479-94

Report Prepared For:
Mr. Dan Russell
PO Box 655
Ridgeland, MS 39158

Report Prepared January 19, 1994 by:
Armstrong Environmental, Inc.
7715 Sovereign Row
Dallas, Texas 75247
(214) 631-0021

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I. INTRODUCTION

A series of tests were performed on the South RTO Exhaust at the Louisiana Pacific facility located in Urania, Louisiana on January 18-19, 1994.

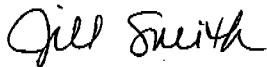
The purpose of this test series was to determine emission rates of Particulate, CO, NOx, VOC and Formaldehyde in terms of lbs/hr.

Testing was performed following procedures detailed in Title 40:Code of Federal Regulations (40:CFR).

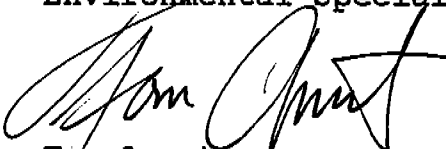
Sampling was performed by Cody Jefferson, Scott Craig, Jerry Salinas, Larry Whicher and Tom Armstrong of Armstrong Environmental, Inc. using an Apex Method 5 sampling train, a Beckman 400A Continuous FID Hydrocarbon analyzer, a Fuji Continuous NDIR CO Analyzer and a TECO Model 10 Continuous NOX Analyzer.

Testing was performed over a two day period, commencing on January 18 at 11:14 am and ending at 5:55 pm and commencing at 11:06 am and ending at 7:10 pm, January 19, 1994.

Submitted by:
Armstrong Environmental Inc.



Jill Smith
Environmental Specialist



Tom Armstrong
President

II. SUMMARY

A series of tests were performed on the Louisiana Pacific South RTO Exhaust at the facility in Urania, LA on January 18-19, 1994.

Testing was performed following procedures detailed in Title 40: Code of Federal Regulations.

The results of this test series are summarized in Table 1-2.

Results indicate the following emission rates:

<u>Run #</u>	<u>1</u>	<u>2</u>	<u>3</u>	<u>Average</u>
Particulate, lbs/hr	6.372	11.69	6.795	8.286
NOX as NO2, lbs/hr	16.74	15.73	13.06	15.18
CO, lbs/hr	0.315	ND	ND	0.105
Formaldehyde, lbs/hr	0.3633	0.4372	0.6224	0.4743
VOC as C3H8, lbs/hr	0.255	ND	ND	0.085

Formaldehyde results reported by telephone via Dan Russell on February 8, 1994.

SUMMARY OF EMISSIONS TEST DATA

Table : 1

Plant : Louisiana Pacific, Urania, LA

Location : South RTO Exhaust - Particulate Train

Operator : C.Jefferson, S.Craig, J.Salinas, L.Whicher, T.Armstrong

Test Date : 18-Jan-94

Repetition :	1	2	3
STACK GAS			
Temperature, F	220.4	225.5	220.8
Velocity, fps	46.37	45.04	44.97
Volume Flow, acfm	108361.7	105251.1	105070.9
scfm	80061.0	76576.4	76971.4
scfh	4803662	4594581	4618286
Moisture, %	6.02%	6.76%	6.64%
CO2, %	0.00	0.00	0.00
O2, %	21.00	21.00	20.00
SAMPLE			
Start Time, hrs:min	11:14 AM	2:58 PM	4:55 PM
Finish Time, hrs:min	12:18 PM	3:59 PM	5:55 PM
Sample Volume, scf	39.399	38.106	38.514
Isokinetic Ratio, %	97.36243	98.45317	98.99711
PARTICULATE			
Sample Weight, mg	23.70	43.97	25.70
Concentration, gr/scf	0.009282	0.017804	0.010296
Emissions, lbs/hr	6.371541	11.69001	6.795145
CARBON MONOXIDE			
Concentration, ppm	0.9045	ND	ND
Emissions, lbs/hr	0.31583	ND	ND
NITROGEN OXIDE AS NO2			
Concentration, ppm	29.245	28.662	23.69
Emissions, lbs/hr	16.77628	15.72621	13.06524

SUMMARY OF EMISSIONS TEST DATA

Table : 2

Plant : Louisiana Pacific, Urania, LA

Location : South RTO Exhaust - Formaldehyde Train

Operator : C.Jefferson, S.Craig, J.Salinas

Test Date : 19-Jan-94

Repetition :	1	2	3
STACK GAS			
Temperature, F	218.3	225.7	224.9
Velocity, fps	47.31	47.49	48.68
Volume Flow, acfm	110535.5	110968.9	113743.9
scfm	81580.8	80953.7	83207.0
scfh	4894848	4857224	4992419
Moisture, %	6.91%	6.99%	6.83%
CO2, %	0.00	0.00	0.00
O2, %	21.00	21.00	21.00
SAMPLE			
Start Time, hrs:min	11:06 AM	4:27 PM	6:10 PM
Finish Time, hrs:min	12:06 PM	5:27 PM	7:10 PM
Sample Volume, scf	73.386	72.510	77.817
Isokinetic Ratio, %	98.16559	97.74506	102.0585
VOC AS C3H8			
Concentration, ppm	0.456	ND	ND
Emissions, lbs/hr	0.254959	ND	ND
FORMALDEHYDE			
Sample Weight, mg	2.47	2.96	4.40
Concentration, ppm	0.95197	1.154605	1.599253
Emissions, lbs/hr	0.363272	0.437211	0.62244

III. PROCEDURES

The procedure for emissions sampling followed USEPA test methods as detailed in Title 40: Code of Federal Regulations. The following methods were used:

Method	Title
1	Sample and Velocity Traverses from Stationary Sources
2	Determination of Stack Gas Velocity and Volumetric Flow (Type S Pitot)
3	Gas Analysis for CO ₂ , O ₂ , Excess Air and Dry Molecular Weight
4	Determination of Moisture Content in Stack Gases
5	Determination of Particulate Emissions from Stationary Sources
7E	Determination of Nitrogen Oxides Emissions from Stationary Sources (Instrument Analyzer Procedure)
10	Determination of Carbon Monoxide Emissions from Stationary Sources
25A	Determination of Total Gaseous Organic Concentration using a Flame Ionization Analyzer

Particulate sampling was performed at 24 points, 2.5 minutes per point, making a total run duration of 60.0 minutes. A 9 foot stainless steel probe was used with a 0.24533 inch ID stainless steel sampling nozzle. Sampling was performed using a "Type S" pitot tube.

Formaldehyde sampling was performed using an Apex Method 5 sampling train with a glass lined probe and a 0.33033 glass nozzle. Sampling was performed isokinetically at 24 points for 60 minutes. Formaldehyde train contained 100 mls of DNPH reagent in each of the first and second impingers, third empty and fourth containing Silica Gel.

CO₂ and O₂ were determined using fyrite analyzers.

Volume flow, moisture and particulates were determined using an Apex Method 5 sampling train with 100mls of distilled water in the first and second impingers, third empty, and 200 grams of silica gel in the fourth impinger.

Carbon monoxide was determined using a Fuji Continuous NDIR CO Analyzer spanned with 402 ppm, 106.7 ppm and 50 ppm EPA Protocol 1 CO gas standards balanced with N₂, +/- 2% Certified.

Nitrogen oxides were determined using a TECO Model 10 Continuous NOX Analyzer spanned with 402.4 ppm, 98.2 ppm and 30.6 ppm EPA Protocol 1 NOX gas standards balanced with N2.

VOC was determined using a Beckman 400A FID analyzer spanned with 203 ppm, 30.4 ppm and 5.5 ppm EPA Protocol 1 Propane gas standards balanced with N2.

Formaldehyde analysis was provided by Mr. Dan Russell, to whom Formaldehyde samples were delivered onsite.

APPENDIX A

PARTICULATE EMISSION TEST SUMMARY

PLANT : Louisiana Pacific, Urania, LA
 DATE : 18-Jan-94
 PLACE : South RTO Exhaust - Particulate Train
 RUN# : 1

TEST DURATION (MINUTES) :	60	LIQUID COLLECTED (mls) :	53.6
NOZZLE DIAMETER (INCH.) :	0.24533	PARTICULATE WEIGHT (Front half mg)	23.7
METER COEFFICIENT (Y) :	0.97853	PARTICULATE WEIGHT (Back half mg)	0
PITOT COEFFICIENT (Cp) :	0.84	STATIC PRESSURE (in. H2O) :	-0.28
GAS METER VOL.(Cu.Ft.) :	38.563	PERCENT CO2 :	0
BAROMETRIC PRESSURE :	30.33	PERCENT O2 :	21
		PERCENT CO :	0

MOLECULAR WEIGHTS

CARBON MONOXIDE :	28	FLUORIDES :	19
VOC AS C3H8 :	44	CHLORIDES :	35.5
NOX AS NO2 :	46		

FOR CIRCULAR STACK

STACK DIAMETER (inch): 84.5
 STACK AREA (Sq.Ft.) : 38.944
 NOZZLE AREA (feet): 0.00033

FOR RECTANGULAR STACK

STACK LENGTH(inches) :
 STACK WIDTH(inches) :
 STACK AREA (Sq.Ft.) : 0

ENTER THE STACK AREA SHOWN ABOVE: 38.944

FLOWS

SAMPLED VOLUME (STD. CU.FT.):	39.3990
VOLUME OF WATER VAPOR (STD. CU.FT.):	2.5230
FRACTIONAL MOISTURE CONTENT (%):	0.0602
DRY BASE:	79.0000
MOLECULAR WT. OF STACK GAS (DRY BASE):	28.8400
MOLECULAR WT. OF STACK GAS (WET BASE):	28.1876

STACK PRESSURE (inch Hg):	30.3094
STACK GAS VELOCITY (ft/sec.):	46.3750
ACTUAL STACK GAS FLOW RATE (ACFM):	108361.744
STANDARD STACK GAS FLOW RATE (SCFH):	4803661.69

PARTICULATE

FRONT HALF

PARTICULATE CONCENTRATION (GR./SCF):	0.0093
PARTICULATE CONCENTRATION (LBS/SCF):	1.33E-06
PARTICULATE EMISSION (LBS/HR):	6.3715

BACK HALF

PARTICULATE CONCENTRATION (GR./SCF):	0.0000
PARTICULATE CONCENTRATION (LBS/SCF):	0.00E+00
PARTICULATE EMISSION (LBS/HR):	0.0000

ISOKINETIC RATIO (%): 97.3624

POINTS	STACK T. deg F	DELTA P	SQ DP	DELTA H	METER T. INLET	METER T. OUTLET	METER T. AVERAGE
1	216	0.66	0.8124	1.58	50	51	50.5
2	220	0.68	0.82462	1.62	46	46	46
3	225	0.64	0.8	1.52	50	47	48.5
4	220	0.62	0.7874	1.48	53	44	48.5
5	219	0.58	0.76158	1.38	54	45	49.5
6	220	0.58	0.76158	1.38	54	46	50
7	223	0.49	0.7	1.17	55	45	50
8	223	0.46	0.67823	1.09	59	46	52.5
9	224	0.55	0.74162	1.31	58	46	52
10	221	0.55	0.74162	1.31	58	46	52
11	219	0.64	0.8	1.52	60	48	54
12	221	0.59	0.76811	1.41	62	49	55.5
13	226	0.73	0.8544	1.74	57	54	55.5
14	218	0.67	0.81854	1.60	60	54	57
15	217	0.68	0.82462	1.62	60	54	57
16	225	0.62	0.7874	1.48	61	53	57
17	218	0.52	0.72111	1.24	62	52	57
18	223	0.45	0.67082	1.07	62	51	56.5
19	216	0.35	0.59161	0.83	62	53	57.5
20	222	0.32	0.56569	0.76	63	51	57
21	226	0.35	0.59161	0.83	64	52	58
22	214	0.38	0.61644	0.90	63	53	58
23	215	0.35	0.59161	0.83	64	53	58.5
24	218	0.31	0.55678	0.74	64	52	58
	220.375		0.7237	1.2671	58.3750	49.6250	54.0000

PARTICULATE EMISSION TEST SUMMARY

PLANT : Louisiana Pacific, Urania, LA
 DATE : 18-Jan-94
 PLACE : South RTO Exhaust - Particulate Train
 RUN# : 2

TEST DURATION (MINUTES) :	60	LIQUID COLLECTED (mls) :	58.7
NOZZLE DIAMETER (INCH.) :	0.24533	PARTICULATE WEIGHT (Front half mg)	43.97
METER COEFFICIENT (Y) :	0.97853	PARTICULATE WEIGHT (Back half mg)	0
PITOT COEFFICIENT (Cp) :	0.84	STATIC PRESSURE (in. H2O) :	-0.28
GAS METER VOL.(Cu.Ft.) :	37.266	PERCENT CO2 :	0
BAROMETRIC PRESSURE :	30.33	PERCENT O2 :	21
		PERCENT CO :	0

MOLECULAR WEIGHTS

CARBON MONOXIDE :	28	FLUORIDES :	19
VOC AS C3H8 :	44	CHLORIDES :	35.5
NOX AS NO2 :	46		

FOR CIRCULAR STACK

STACK DIAMETER (inch): 84.5
 STACK AREA (Sq.Ft.) : 38.944
 NOZZLE AREA (feet): 0.00033

FOR RECTANGULAR STACK

STACK LENGTH(inches) :
 STACK WIDTH(inches) :
 STACK AREA (Sq.Ft.) : 0

ENTER THE STACK AREA SHOWN ABOVE: 38.944

FLOWS

SAMPLED VOLUME (STD. CU.FT.):	38.1062
VOLUME OF WATER VAPOR (STD. CU.FT.):	2.7630
FRACTIONAL MOISTURE CONTENT (%):	0.0676
DRY BASE:	79.0000
MOLECULAR WT. OF STACK GAS (DRY BASE):	28.8400
MOLECULAR WT. OF STACK GAS (WET BASE):	28.1072

STACK PRESSURE (inch Hg):	30.3094
STACK GAS VELOCITY (ft/sec.):	45.0437
ACTUAL STACK GAS FLOW RATE (ACFM):	105251.056
STANDARD STACK GAS FLOW RATE (SCFH):	4594581.11

PARTICULATE

FRONT HALF

PARTICULATE CONCENTRATION (GR./SCF):	0.0178
PARTICULATE CONCENTRATION (LBS/SCF):	2.54E-06
PARTICULATE EMISSION (LBS/HR):	11.6900

BACK HALF

PARTICULATE CONCENTRATION (GR./SCF):	0.0000
PARTICULATE CONCENTRATION (LBS/SCF):	0.00E+00
PARTICULATE EMISSION (LBS/HR):	0.0000

ISOKINETIC RATIO (%):

98.4532

POINTS	STACK T. deg F	DELTA P	SQUAR D.P	DELTA H	METER T. INLET	METER T. OUTLET	METER T. AVERAGE
1	215	0.59	0.76811	1.41	49	48	48.5
2	224	0.58	0.76158	1.38	49	46	47.5
3	221	0.59	0.76811	1.41	52	45	48.5
4	223	0.56	0.74833	1.33	54	46	50
5	223	0.46	0.67823	1.09	57	44	50.5
6	232	0.52	0.72111	1.24	58	44	51
7	228	0.39	0.6245	0.93	59	43	51
8	225	0.41	0.64031	0.97	60	44	52
9	234	0.52	0.72111	1.24	62	44	53
10	232	0.55	0.74162	1.31	64	45	54.5
11	230	0.64	0.8	1.52	64	46	55
12	221	0.60	0.7746	1.43	63	48	55.5
13	230	0.72	0.84853	1.72	59	50	54.5
14	234	0.67	0.81854	1.60	61	51	56
15	224	0.67	0.81854	1.60	61	49	55
16	223	0.55	0.74162	1.31	62	50	56
17	227	0.46	0.67823	1.09	62	49	55.5
18	230	0.39	0.6245	0.93	62	49	55.5
19	228	0.33	0.57446	0.78	62	50	56
20	227	0.31	0.55678	0.74	63	50	56.5
21	223	0.32	0.56569	0.76	62	49	55.5
22	221	0.35	0.59161	0.83	61	49	55
23	219	0.38	0.61644	0.90	63	48	55.5
24	217	0.36	0.6	0.86	62	48	55
	225.4583		0.6993	1.1825	59.6250	47.2917	53.4583

PARTICULATE EMISSION TEST SUMMARY

PLANT : Louisiana Pacific, Urania, LA
DATE : 18-Jan-94
PLACE : South RTO Exhaust - Particulate Train
RUN# : 3

TEST DURATION (MINUTES) :	60	LIQUID COLLECTED (mls) :	58.2
NOZZLE DIAMETER (INCH.) :	0.24533	PARTICULATE WEIGHT (Front half mg)	25.7
METER COEFFICIENT (Y) :	0.97853	PARTICULATE WEIGHT (Back half mg)	0
PITOT COEFFICIENT (Cp) :	0.84	STATIC PRESSURE (in. H2O) :	-0.28
GAS METER VOL.(Cu.Ft.) :	37.289	PERCENT CO2 :	0
BAROMETRIC PRESSURE :	30.29	PERCENT O2 :	20
		PERCENT CO :	0

MOLECULAR WEIGHTS

CARBON MONOXIDE :	28	FLUORIDES :	19
VOC AS C3H8 :	44	CHLORIDES :	35.5
NOX AS NO2 :	46		

FOR CIRCULAR STACK

STACK DIAMETER (inch): 84.5
STACK AREA (Sq.Ft.) : 38.944
NOZZLE AREA (feet): 0.00033

FOR RECTANGULAR STACK

STACK LENGTH(inchs) :
STACK WIDTH(inchs) :
STACK AREA (Sq.Ft.) :

0

ENTER THE STACK AREA SHOWN ABOVE: 38.944

FLOWS

SAMPLED VOLUME (STD. CU.FT.):	38.5145
VOLUME OF WATER VAPOR (STD. CU.FT.):	2.7395
FRACTIONAL MOISTURE CONTENT (%):	0.0664
DRY BASE:	80.0000
MOLECULAR WT. OF STACK GAS (DRY BASE):	28.8000
MOLECULAR WT. OF STACK GAS (WET BASE):	28.0828

STACK PRESSURE (inch Hg):	30.2694
STACK GAS VELOCITY (ft/sec.):	44.9666
ACTUAL STACK GAS FLOW RATE (ACFM):	105070.902
STANDARD STACK GAS FLOW RATE (SCFH):	4618285.92

PARTICULATE

FRONT HALF

PARTICULATE CONCENTRATION (GR./SCF):	0.0103
PARTICULATE CONCENTRATION (LBS/SCF):	1.47E-06
PARTICULATE EMISSION (LBS/HR):	6.7951

BACK HALF

PARTICULATE CONCENTRATION (GR./SCF):	0.0000
PARTICULATE CONCENTRATION (LBS/SCF):	0.00E+00
PARTICULATE EMISSION (LBS/HR):	0.0000

ISOKINETIC RATIO (%): 98.9971

POINTS	STACK T. deg F	DELTA P	SQUAR D.P	DELTA H	METER T. INLET	METER T. OUTLET	METER T. AVERAGE
1	217	0.57	0.75498	1.36	51	50	50.5
2	222	0.59	0.76811	1.41	43	45	44
3	225	0.55	0.74162	1.31	44	43	43.5
4	219	0.54	0.73485	1.29	48	40	44
5	220	0.49	0.7	1.17	50	41	45.5
6	222	0.45	0.67082	1.07	53	38	45.5
7	221	0.38	0.61644	0.90	52	38	45
8	218	0.43	0.65574	1.02	54	38	46
9	217	0.52	0.72111	1.24	54	39	46.5
10	222	0.65	0.80623	1.55	55	39	47
11	220	0.62	0.7874	1.48	55	39	47
12	225	0.60	0.7746	1.43	56	39	47.5
13	222	0.79	0.88882	1.88	50	43	46.5
14	220	0.74	0.86023	1.76	54	43	48.5
15	221	0.65	0.80623	1.55	56	45	50.5
16	220	0.52	0.72111	1.24	58	44	51
17	220	0.38	0.61644	0.90	57	44	50.5
18	223	0.40	0.63246	0.95	57	42	49.5
19	221	0.34	0.5831	0.81	56	42	49
20	218	0.31	0.55678	0.74	57	42	49.5
21	222	0.31	0.55678	0.74	56	42	49
22	219	0.37	0.60828	0.88	56	41	48.5
23	221	0.42	0.64807	1.00	57	43	50
24	223	0.34	0.5831	0.81	57	42	49.5
	220.75		0.6997	1.1871	53.5833	41.7500	47.6667

PARTICULATE EMISSION TEST SUMMARY

PLANT : Louisiana Pacific, Urania, LA
 DATE : 19-Jan-94
 PLACE : South RTO Exhaust - Formaldehyde Train
 RUN# : 1

TEST DURATION (MINUTES) :	60	LIQUID COLLECTED (mls) :	115.7
NOZZLE DIAMETER (INCH.) :	0.33033	PARTICULATE WEIGHT (Front half mg)	0
METER COEFFICIENT (Y) :	0.97853	PARTICULATE WEIGHT (Back half mg)	0
PITOT COEFFICIENT (Cp) :	0.84	STATIC PRESSURE (in. H2O) :	-0.33
GAS METER VOL.(Cu.Ft.) :	72.13	PERCENT CO2 :	0
BAROMETRIC PRESSURE :	30.5	PERCENT O2 :	21
		PERCENT CO :	0

MOLECULAR WEIGHTS

CARBON MONOXIDE :	28	FLUORIDES :	19
VOC AS C3H8 :	44	CHLORIDES :	35.5
NOX AS NO2 :	46		

FOR CIRCULAR STACK

STACK DIAMETER (inch): 84.5
 STACK AREA (Sq.Ft.) : 38.944
 NOZZLE AREA (feet): 0.0006

FOR RECTANGULAR STACK

STACK LENGTH(inches) :
 STACK WIDTH(inches) :
 STACK AREA (Sq.Ft.) : 0

ENTER THE STACK AREA SHOWN ABOVE: 38.944

FLOWS

SAMPLED VOLUME (STD. CU.FT.):	73.3860
VOLUME OF WATER VAPOR (STD. CU.FT.):	5.4460
FRACTIONAL MOISTURE CONTENT (%):	0.0691
DRY BASE:	79.0000
MOLECULAR WT. OF STACK GAS (DRY BASE):	28.8400
MOLECULAR WT. OF STACK GAS (WET BASE):	28.0911
STACK PRESSURE (inch Hg):	30.4757
STACK GAS VELOCITY (ft/sec.):	47.3053
ACTUAL STACK GAS FLOW RATE (ACFM):	110535.539
STANDARD STACK GAS FLOW RATE (SCFH):	4894848.36

ISOKINETIC RATIO (%): 98.1656

POINTS	STACK T. deg F	DELTA P	SQ DP	DELTA H	METER T. INLET	METER T. OUTLET	METER T. AVERAGE
1	215	0.72	0.84853	5.50	62	63	62.5
2	218	0.70	0.83666	5.40	63	62	62.5
3	220	0.65	0.80623	5.04	65	63	64
4	220	0.61	0.78102	4.73	66	63	64.5
5	222.3	0.62	0.7874	4.80	68	63	65.5
6	223	0.52	0.72111	5.10	69	64	66.5
7	221	0.43	0.65574	4.22	69	64	66.5
8	219	0.48	0.69282	3.72	69	65	67
9	220	0.50	0.70711	3.87	69	65	67
10	206	0.61	0.78102	4.73	55	57	56
11	206	0.64	0.8	4.96	57	59	58
12	208	0.57	0.75498	4.42	58	59	58.5
13	228	0.91	0.95394	7.05	58	58	58
14	221	0.82	0.90554	6.35	62	59	60.5
15	217	0.74	0.86023	5.73	63	59	61
16	220	0.65	0.80623	5.04	64	59	61.5
17	221	0.60	0.7746	4.65	65	59	62
18	218	0.55	0.74162	4.26	66	60	63
19	219	0.41	0.64031	3.17	67	60	63.5
20	223	0.32	0.56569	2.48	67	60	63.5
21	221	0.33	0.57446	2.55	68	61	64.5
22	220	0.37	0.60828	2.86	68	61	64.5
23	223	0.35	0.59161	2.71	69	61	65
24	211	0.32	0.56569	2.48	69	62	65.5
	218.3458		0.7400	4.4092	64.8333	61.0833	62.9583

PARTICULATE EMISSION TEST SUMMARY

PLANT : Louisiana Pacific, Urania, LA
 DATE : 19-Jan-94
 PLACE : South RTO Exhaust - Formaldehyde Train
 RUN# : 2

TEST DURATION (MINUTES) :	60	LIQUID COLLECTED (mls) :	115.7
NOZZLE DIAMETER (INCH.) :	0.33033	PARTICULATE WEIGHT (Front half mg)	0
METER COEFFICIENT (Y) :	0.97853	PARTICULATE WEIGHT (Back half mg)	0
PITOT COEFFICIENT (Cp) :	0.84	STATIC PRESSURE (in. H2O) :	-0.33
GAS METER VOL.(Cu.Ft.) :	72.13	PERCENT CO2 :	0
BAROMETRIC PRESSURE :	30.5	PERCENT O2 :	21
		PERCENT CO :	0

MOLECULAR WEIGHTS

CARBON MONOXIDE :	28	FLUORIDES :	19
VOC AS C3H8 :	44	CHLORIDES :	35.5
NOX AS NO2 :	46		

FOR CIRCULAR STACK

STACK DIAMETER (inch):	84.5	FOR RECTANGULAR STACK	
STACK AREA (Sq.Ft.) :	38.944	STACK LENGTH(inches) :	
NOZZLE AREA (feet):	0.0006	STACK WIDTH(inches) :	
		STACK AREA (Sq.Ft.) :	0

ENTER THE STACK AREA SHOWN ABOVE: 38.944

FLOWS

SAMPLED VOLUME (STD. CU.FT.):	72.5100
VOLUME OF WATER VAPOR (STD. CU.FT.):	5.4460
FRACTIONAL MOISTURE CONTENT (%):	0.0699
DRY BASE:	79.0000
MOLECULAR WT. OF STACK GAS (DRY BASE):	28.8400
MOLECULAR WT. OF STACK GAS (WET BASE):	28.0827

STACK PRESSURE (inch Hg):	30.4757
STACK GAS VELOCITY (ft/sec.):	47.4908
ACTUAL STACK GAS FLOW RATE (ACFM):	110968.931
STANDARD STACK GAS FLOW RATE (SCFH):	4857223.65

ISOKINETIC RATIO (%):	97.7451
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POINTS	STACK T. deg F	DELTA P	SQUAR D.P	DELTA H	METER T. INLET	METER T. OUTLET	METER T. AVERAGE
1	225	0.71	0.84261	5.50	59	58	58.5
2	230	0.75	0.86603	5.80	59	59	59
3	220	0.68	0.82462	5.20	64	59	61.5
4	222	0.66	0.8124	5.10	68	59	63.5
5	220	0.64	0.8	4.90	71	59	65
6	229	0.65	0.80623	5.00	73	60	66.5
7	222	0.43	0.65574	3.30	75	60	67.5
8	225	0.43	0.65574	3.30	76	60	68
9	227	0.51	0.71414	3.90	77	61	69
10	222	0.54	0.73485	4.10	77	61	69
11	232	0.57	0.75498	4.40	79	62	70.5
12	231	0.56	0.74833	4.60	80	62	71
13	226	0.84	0.91652	7.00	71	61	66
14	223	0.84	0.91652	7.00	76	63	69.5
15	231	0.74	0.86023	6.10	79	64	71.5
16	230	0.67	0.81854	5.50	81	65	73
17	228	0.58	0.76158	4.70	82	65	73.5
18	227	0.47	0.68557	3.80	83	66	74.5
19	226	0.44	0.66332	3.60	83	66	74.5
20	228	0.34	0.5831	2.80	83	67	75
21	220	0.35	0.59161	2.80	81	67	74
22	229	0.38	0.61644	3.10	82	67	74.5
23	223	0.34	0.5831	2.80	81	67	74
24	221	0.27	0.51962	2.20	81	68	74.5
	225.7083		0.7388	4.4375	75.8750	62.7500	69.3125

PARTICULATE EMISSION TEST SUMMARY

PLANT : Louisiana Pacific, Urania, LA
 DATE : 19-Jan-94
 PLACE : South RTO Exhaust - Formaldehyde Train
 RUN# : 3

TEST DURATION (MINUTES) :	60	LIQUID COLLECTED (mls) :	121.2
NOZZLE DIAMETER (INCH.) :	0.33033	PARTICULATE WEIGHT (Front half mg)	0
METER COEFFICIENT (Y) :	0.97853	PARTICULATE WEIGHT (Back half mg)	0
PITOT COEFFICIENT (Cp) :	0.84	STATIC PRESSURE (in. H2O) :	-0.36
GAS METER VOL.(Cu.Ft.) :	75.035	PERCENT CO2 :	0
BAROMETRIC PRESSURE :	30.5	PERCENT O2 :	21
		PERCENT CO :	0

MOLECULAR WEIGHTS

CARBON MONOXIDE :	28	FLUORIDES :	19
VOC AS C3H8 :	44	CHLORIDES :	35.5
NOX AS NO2 :	46		

FOR CIRCULAR STACK

STACK DIAMETER (inch):	84.5	FOR RECTANGULAR STACK	
STACK AREA (Sq.Ft.) :	38.944	STACK LENGTH(inchs) :	
NOZZLE AREA (feet):	0.0006	STACK WIDTH(inchs) :	
		STACK AREA (Sq.Ft.) :	0

ENTER THE STACK AREA SHOWN ABOVE: 38.944

FLOWS

SAMPLED VOLUME (STD. CU.FT.):	77.8171
VOLUME OF WATER VAPOR (STD. CU.FT.):	5.7049
FRACTIONAL MOISTURE CONTENT (%):	0.0683
DRY BASE:	79.0000
MOLECULAR WT. OF STACK GAS (DRY BASE):	28.8400
MOLECULAR WT. OF STACK GAS (WET BASE):	28.0996

STACK PRESSURE (inch Hg):	30.4735
STACK GAS VELOCITY (ft/sec.):	48.6784
ACTUAL STACK GAS FLOW RATE (ACFM):	113743.92
STANDARD STACK GAS FLOW RATE (SCFH):	4992419.15

ISOKINETIC RATIO (%): 102.0585

POINTS	STACK T. deg F	DELTA P	SQUAR D.P	DELTA H	METER T. INLET	METER T. OUTLET	METER T. AVERAGE
1	227	0.74	0.86023	6.10	59	59	59
2	223	0.71	0.84261	5.80	54	56	55
3	227	0.71	0.84261	5.80	55	56	55.5
4	218	0.73	0.8544	6.00	55	55	55
5	222	0.62	0.7874	5.10	55	55	55
6	220	0.65	0.80623	5.30	55	55	55
7	224	0.46	0.67823	3.70	54	54	54
8	228	0.49	0.7	4.00	54	54	54
9	224	0.55	0.74162	4.50	53	53	53
10	223	0.62	0.7874	5.10	58	53	55.5
11	225	0.64	0.8	5.20	58	53	55.5
12	226	0.57	0.75498	4.70	58	53	55.5
13	228	0.92	0.95917	7.50	52	50	51
14	232	0.95	0.97468	7.80	59	50	54.5
15	224	0.81	0.9	6.60	50	50	50
16	230	0.68	0.82462	5.60	50	50	50
17	230	0.56	0.74833	4.60	50	50	50
18	221	0.52	0.72111	4.20	51	49	50
19	222	0.38	0.61644	3.10	54	49	51.5
20	224	0.39	0.6245	3.20	55	49	52
21	225	0.37	0.60828	3.00	57	49	53
22	223	0.35	0.59161	2.80	58	49	53.5
23	225	0.33	0.57446	2.70	58	49	53.5
24	227	0.35	0.59161	2.80	58	49	53.5
	224.9167		0.7579	4.8000	55.0000	52.0417	53.5208

APPENDIX B

PARTICULATE ANALYTICAL DATA FORM

Company: Smith Uran, Co. La. Run Number: R. FW

Location: RTO 5, EX Density(Pa.) _____

Date: 1-18-94

Liquid Level Marked? ☒

Blank Concentration(Ca) _____

Rinse Volume(Vaw) 205 ml Isobone

Residue in Rinse(Wa)=Ca*Vaw*Pa _____

Date of Weighing 1-21-94 Gross Wt. 107.9296

Date of Weighing _____ Gross Wt. 107.9296

Average Gross Wt. 107.9296

Less Blank Residue(Wa) _____

Tare Wt. 107.9168

Weight of Particulate in Rinse 0.0128 = 12.8 mg

Date of Weighing 1-21-94 Gross Filter Wt. 0.46865

Date of Weighing _____ Gross Filter Wt. 0.46867

Average Gross Wt. 0.46866

Filter Tare Wt. 0.45942

Weight of Particulate on Filter 0.00924 9.24 mg

~~Total~~ Weight of Particulate 1.66 mg

Petri Dish

23.7 mg.

PARTICULATE ANALYTICAL DATA FORM

Company: Smith, Urvana La Run Number: R2 PW

Location: RTO S. Ex Density(Pa.) _____

Date: 1-18-94

Liquid Level Marked? ✓

Blank Concentration(Ca) _____

Rinse Volume(Vaw) 130 ml Acetone

Residue in Rinse(Wa) = $Ca \times Vaw \times Pa$ _____

Date of Weighing 1-21-94 Gross Wt. 104.2847

Date of Weighing _____ Gross Wt. 104.2845

Average Gross Wt. 104.2846

Less Blank Residue(Wa) _____

Tare Wt. 104.2536

Weight of Particulate in Rinse 0.0310 31.0 mg

Date of Weighing 1-21-94 Gross Filter Wt. 0.47500

Date of Weighing _____ Gross Filter Wt. 0.47500

Average Gross Wt. 0.47500

Filter Tare Wt. 0.46564

Weight of Particulate on Filter 0.0100 10.0 mg

Total Weight of Particulate 2.97 mg

43.97 mg

PARTICULATE ANALYTICAL DATA FORM

Company: Smith Warrick La Run Number: R3 PL

Location: RTD S, Ex. Density(Pa.) _____

Date: 1-18-94

Liquid Level Marked? ✓

Blank Concentration(Ca) _____

Rinse Volume(Vaw) 230 ml Acetone

Residue in Rinse(Wa) = $Ca * Vaw * Pa$ _____

Date of Weighing 1-21-94 Gross Wt. 106.5590

Date of Weighing _____ Gross Wt. 106.5591

Average Gross Wt. 106.5590

Less Blank Residue(Wa) _____

Tare Wt. 106.5491

Weight of Particulate in Rinse 0.0099 g 9.9 mg

Date of Weighing 1-21-94 Gross Filter Wt. 0.47250

Date of Weighing _____ Gross Filter Wt. 0.47250

Average Gross Wt. 0.47250

Filter Tare Wt. 0.45922

Weight of Particulate on Filter 0.01328 13.28 mcg

Total Weight of Particulate 2.59 mcg

25.7 mg

ACETONE BLANK ANALYTICAL DATA FORM

PLANT: Smith Co.
SAMPLE LOCATION: Blank RTO S. Ex
LIQUID LEVEL MARKED? ☒
BLANK VOLUME (Pa): 75ml

DATE OF WEIGHING 1-21-94 GROSS WEIGHT 99.9579
DATE OF WEIGHING _____ GROSS WEIGHT 99.9581
AVERAGE GROSS WEIGHT 99.9580
TARE WEIGHT 99.9584
WEIGHT OF BLANK (ma) 0.0000

$$Ca = \frac{ma}{Va Pa} = \text{_____ mg/g}$$

Note: In no case should a blank residue greater than 0.01 mg/g or 0.001% of the blank weight be subtracted from the sample weight.

Smith RTO Ex 1-18-94

Petri Dish Wash

wt

net

Tare

$$R_1 \quad .16992g \quad .17251g \quad 0.00259g = 2.59mg$$

$$R_2 \quad .15531g \quad 0.15697g \quad 0.00166g = 1.66mg$$

$$R_3 \quad .15713g \quad 0.16010g \quad 0.00297g = 2.97mg$$

APPENDIX C

PARTICULATE FIELD DATA

$T_m = 40$
 $T_s = 220$

PLANT: LP Uvania
DATE: 1-18-94
REPETITION: 1

$V_{mstd} = 39.681$ 2.2495
 $V_{wstd} = 2.633$
 $B_{ws} = .06223$
 $V_{el} = 45.29$
 $I = 100.14\%$

STD 0 = .885
STD 1 = 3.0
STD 2 = 2.5

LOCATION: South 200 EX - Plant
OPERATOR: G. SG. J. L. W. (TA) TRAIN
STACK #: EX
SAMPLE BOX #: 9
METER BOX #: 7
AMBIENT TEMPERATURE: 75°
BAROMETRIC PRESSURE: 30.33
ASSUMED MOISTURE: 7%
PROBE LENGTH: 9' 8" STAINLESS
NOZZLE DIAMETER: .245, .245, .246 = .2453 = .00833 ft
STACK DIAMETER: 84.5" = 7.04 ft
METER H: 1.67822
C FACTOR: .84
METER CO-EFFICIENT: .97853

IMPINGERS

	Initial	Final
#1: 100 mL	1.20	136
#2: 100 mL		112
#3: —		20.56
#4: 200 g SG		53.6
#5: —		56

COMMENTS:

$\frac{CO_2}{0.0\%}$ $\frac{O_2}{21.0\%}$ 2.633
39.681

FILTER TARE: .45942 g
PRE-TEST LEAK CHECK

Meter: .013 Cu. ft. 15 in. HG
Pitots: in. H2O

POST-TEST LEAK CHECK

Meter: .016 Cu. ft. 7 in. HG
Pitots: in. H2O

Temp
210-220
32

.52
.52
.50
.48
.45
.37
.36
.38
.44
.52
.56
.55
.65
.68
.65
.63
.51
.42
.38
.35
.35
.37
.37
.31

		STATIC PRES.	Ts °F	ΔP	√ΔP	ΔH	Vm FT.³	Tm INLET	Tm OUTLET	OVEN TEMP.	IMP. OUTLET TEMP.	VACUUM (IN H ₂ O)
A	1	11.14	1216	.61		1.58	189.950	50	51	250	30	30
	2	1.32	220	.68		1.62	191.753	46	46	253	30	30
	3		225	.64		1.52	193.585	50	47	256	31	30
	4		220	.62		1.48	195.360	53	44	247	30	30
	5		249	.58		1.38	197.109	54	45	250	30	30
	6		220	.58		1.38	198.861	54	46	251	31	30
	7		223	.49		1.17	200.492	55	45	253	30	1.6
	8		223	.46		1.09	202.046	59	46	247	31	3.0
	9		224	.55		1.31	203.552	58	46	243	31	3.0
	10		221	.55		1.31	205.108	58	46	245	31	3.0
	11		214	.64		1.52	206.945	60	48	247	31	3.0
	12		221	.59		1.41	208.622	62	49	251	31	3.0
B	1	11.55	226	.73		1.74	210.327	57	54	254	31	2.0
	2		218	.67		1.60	212.224	60	54	253	30	2.0
	3		217	.68		1.62	214.042	60	54	253	32	3.0
	4		225	.62		1.48	215.873	61	53	250	31	3.0
	5		218	.52		1.24	217.621	62	53	247	31	3.0
	6		223	.45		1.07	219.222	62	51	248	31	3.0
	7		211	.35		.83	220.711	62	53	248	31	3.0
	8		222	.32		.76	222.025	63	51	249	31	3.0
	9		226	.25		.83	223.281	64	52	251	32	2.0
	10		214	.38		.95	24.595	63	53	251	32	3.0
	11		215	.35		.89	25.903	64	53	253	32	2.0
	12		218	.31		.74	27.271	64	52	256	33	3.0
							225.513					
AV			1220.4	.53208	1.7237		138.563					

PARTICULATE FIELD DATA

PLANT: LP
DATE: 1-18-94
REPETITION: 2

WSP: 51.39
V₂: 45.40
25- 77.15

LOCATION: South RTO Ex - PAINT TRAIN

OPERATOR:
STACK #: Ex
SAMPLE BOX #: 8
METER BOX #: 7
AMBIENT TEMPERATURE: 35
BAROMETRIC PRESSURE: 30.33
ASSUMED MOISTURE: 7%
PROBE LENGTH: 9'
NOZZLE DIAMETER: .24533"
STACK DIAMETER: 84.5"
METER H: 1.67822
C FACTOR: .84
METER CO-EFFICIENT: .97853

IMPINGERS

	Initial	Final
#1: 100 mls	> 420	146
#2: 100 mls		106
#3: —		206.7
#4: 200 g	96	58.7
#5:		

COMMENTS:

CO₂ 0%
O₂ 21%

FILTER TARE: .46564 g
PRE-TEST LEAK CHECK

Meter: 0.005 Cu. ft. 15 in. HG
Pitots: ✓ in. H2O

POST-TEST LEAK CHECK

Meter: 0.00 Cu. ft. 5 in. HG
Pitots: ✓ in. H2O

	Θ	STATIC PRES.	Ts °F	ΔP	√ΔP	ΔH	Vm FT.3	Tm INLET	Tm OUTLET	OVEN TEMP.	IMP. OUTLET TEMP.	VACUUM (IN H ₂ O)
A1	2:58		215	.59		1.41	229.091	49	48	256	34	2
2			224	.58		1.38	230.796	49	46	259	35	2
3			221	.59		1.41	232.497	52	45	258	34	2
4			223	.56		1.33	234.193	54	46	261	36	2
5			223	.46		1.09	235.885	57	44	258	34	2
6	7.28		232	.52		1.24	237.361	58	44	257	35	2
7			228	.39		.93	238.962	59	43	257	37	2
8			225	.41		.97	240.348	60	44	253	33	2
9			234	.52		1.24	241.770	62	44	257	33	2
10			232	.55		1.31	243.372	64	45	249	35	2
11			230	.64		1.32	245.018	64	46	253	34	3
12			221	.60		1.43	246.795	63	48	251	33	3
B1			230	.72		1.72	248.515	59	50	250	33	4
2			234	.67		1.60	250.399	61	51	257	33	4
3			224	.67		1.60	252.217	61	49	258	32	4
4			223	.55		1.31	254.034	62	50	257	33	3
5			227	.46		1.09	255.681	62	49	252	31	3
6			230	.39		.93	257.187	62	49	251	31	3
7			228	.33		.78	258.574	62	50	258	31	2
8			227	.31		.74	259.849	63	50	254	31	2
9			223	.32		.76	261.086	62	49	253	31	2
10			221	.35		.83	262.342	61	49	250	30	2
11			219	.38		.90	263.655	63	48	251	30	2
12			217	.36		.86	265.024	62	48	250	29	2
							266.357					
AV			225.5	.49667	1.69927	1.183	37.2661	53.51				

PARTICULATE FIELD DATA

PLANT: LP
DATE: 1-18-94
REPETITION: 3

LOCATION: RTO South Ex. - DANT. TRAIN
OPERATOR: JS/SC
STACK #: RTO South Ex.
SAMPLE BOX #: 7
METER BOX #: 7
AMBIENT TEMPERATURE: 35
BAROMETRIC PRESSURE: 30.29
ASSUMED MOISTURE: 7%
PROBE LENGTH: 9
NOZZLE DIAMETER: .24533"
STACK DIAMETER: 84.5"
METER H: 1.87822
C FACTOR: .84
METER CO-EFFICIENT: .97853

IMPINGERS

	Initial	Final
#1: 100 mls		132 mls
#2: 100 mls	> H ₂ O	120 mls
#3: —		206.2
#4: 200 gr Sk		58.2
#5:		

COMMENTS:

CO₂ O₂
0% 20%

FILTER TARE: .45922
PRE-TEST LEAK CHECK

Meter: 0.00 Cu. ft. 15 in. HG
Pitots: ✓ in. H2O

POST-TEST LEAK CHECK

Meter: // Cu. ft. 5 in. HG
Pitots: // in. H2O

	θ	STATIC PRES.	Ts OF	ΔP	√ΔP	ΔH	Vm FT./S	Tm INLET	Tm OUTLET	OVEN TEMP	IMP OUTLET TEMP	VACUUM (IN H ₂ O)
A	4:59		217	.57		1.36	266.505	51	50	257	29	15
2			222	.59		1.41	268.185	43	45	254	29	2
3	5:04	-.28	225	.55		1.31	269.870	44	43	249	29	2
4			219	.54		1.29	271.610	48	40	250	29	2
5	5:09		220	.49		1.17	273.135	50	41	247	29	2
6			222	.45		1.07	274.772	53	38	248	28	2
7	5:14		221	.38		.90	276.378	52	38	246	28	2
8			218	.43		1.02	277.845	54	38	245	28	2
9	5:19		217	.52		1.24	279.250	54	39	246	28	2
10			222	.65		1.55	280.710	55	39	242	28	2
11	5:24		220	.62		1.48	282.325	55	39	244	28	2
12			225	.60		1.43	283.970	56	39	242	28	2
B	5:31		222	.79		1.88	285.697	50	43	254	28	2
2			220	.74		1.76	287.380	54	43	257	28	2
3	5:36		221	.65		1.55	289.475	56	45	258	28	2
4			220	.52		1.24	291.395	58	44	259	28	2
5	5:41		220	.38		.90	293.165	57	44	255	28	2.5
6			223	.40		.95	294.690	57	42	255	28	2
7	5:46		221	.34		.81	296.060	56	42	260	28	2
8			218	.31		.74	297.335	57	42	256	28	2
9	5:51		222	.31		.74	298.935	56	42	255	28	7.5
10			219	.37		.88	299.720	56	41	252	28	15
11	5:56		221	.42		1.00	301.012	57	43	256	28	1
12	5:58:30		223	.34		.81	302.513	57	42	257	28	1
							303.794					
AV							37.2891					

PARTICULATE FIELD DATA

PLANT: LP
DATE: 1-19-94
REPETITION: 1

STD 0 1.64184

STD 0 = 1.660
STD 1 = 3.029
STD 2 = 2.5

LOCATION: RTO South Ex Formaldehyde TRAIN
OPERATOR: JS, CS, SC
STACK #: EX
SAMPLE BOX #: 9
METER BOX #: 7
AMBIENT TEMPERATURE: 25°
BAROMETRIC PRESSURE: 30.5
ASSUMED MOISTURE: 6%
PROBE LENGTH: 11' - 11 FT GLASS
NOZZLE DIAMETER: .330, .330, .331 (.33033)
STACK DIAMETER: 84.5" (36.944 ft²) (.00060)
METER H: 1.67822
C FACTOR: .84
METER CO-EFFICIENT: .97853

IMPINGERS

	Initial	Final
#1: 100 ml		176
#2: 100 ml > DNPH		115
#3: —		1
#4: 200 gr SL		217.1
#5:		109.10

COMMENTS:

CO₂ 0%
O₂ 21%

FILTER TARE: N/A

PRE-TEST LEAK CHECK

Meter: 1005 Cu. ft. / 5 in. HG
Pitots: ✓ 185 in. H2O
175

POST-TEST LEAK CHECK

Meter: 0.00 ✓ Cu. ft. / 8 in. HG
Pitots: in. H2O

	θ	STATIC PRES.	Ts °F	ΔP	√ΔP	ΔH	Vm FT.³	Tm INLET	Tm OUTLET	OVEN TEMP.	IMP OUTLET TEMP.	VACUUM (IN H ₂ O)
A1	11.06		215	.72		5.5	306.719	62	63	258	30	15
2			218	.70		5.4	310.113	63	62	257	30	15
3			220	.65		5.04	313.459	65	63	262	30	15
4		-.38	220	.61		4.73	316.684	66	63	261	30	15
5			222.3	.62		4.80	319.808	68	63	258	30	15
6			223	.52		5.10	322.458	69	64	257	30	15
7			221	.43		4.22	326.203	69	64	259	30	15
8			219	.48		3.72	329.154	69	65	263	30	15
9	11/33 / 18.35		220	.50		3.87	331.925	69	65	265	30	15
10			206	.61		4.73	334.753	55	57	264	30	16
11			206	.64		4.96	337.878	57	59	261	30	15
12			208	.57		4.42	341.078	58	59	258	30	15
131			228	.91		7.05	344.097	58	58	258	30	15
2			221	.82		6.35	347.913	62	59	256	30	16
3			217	.74		5.73	351.535	63	59	258	30	16
4			220	.65		5.04	354.976	64	59	262	30	16
5			221	.60		4.65	358.201	65	59	261	30	16
6		-.36	218	.55		4.26	361.300	66	60	263	30	16
7			219	.41		3.17	364.266	67	60	260	30	16
8			223	.32		2.48	366.827	67	60	269	30	16
9			221	.33		2.55	369.090	68	61	268	30	16
10			220	.37		2.86	371.388	68	61	261	30	16
11			223	.35		2.71	373.821	69	61	263	30	16
12			211	.32		2.48	376.187	69	62	260	30	16
							378.450					
AV		-.37	218.3	1.55917		14.409	71.731	63.01				

Vel = 47.96

20.07 m/s

6.5% moisture
1-605 = .935

vmstl = 72.974
27

Ts = 678
Ta = 523

WAB = 28.84
MS = 28.13
20.20.47

TSO = 95.41
20.20.47
MS = 857.199

PARTICULATE FIELD DATA

0-1

PLANT: LP
DATE: 1-19-94
REPETITION: 2

LOCATION: RTO South E6 FORM. TMAN
OPERATOR:
STACK #: Exhaust
SAMPLE BOX #: 9
METER BOX #: 7
AMBIENT TEMPERATURE: 45
BAROMETRIC PRESSURE: 30.5
ASSUMED MOISTURE: 6%
PROBE LENGTH: 11'
NOZZLE DIAMETER: .330, .330, .331
STACK DIAMETER: 84.5"
METER H: 1.67822
C FACTOR: .84
METER CO-EFFICIENT: .97853

IMPINGERS

	Initial	Final
#1: 100 mls		128
#2: 100 mls > DNPH		151
#3: —		18
#4: 200 gr SL		218.7
#5:		115.7

COMMENTS:

CO₂ 0%
O₂ 21%

FILTER TARE: N/A
PRE-TEST LEAK CHECK

Meter: 0.00 Cu. ft. 15 in. HG
Pitots: in. H2O

POST-TEST LEAK CHECK

Meter: 0.00 Cu. ft. 5 in. HG
Pitots: in. H2O

	⊖	STATIC PRES.	Ts °F	ΔP	√ΔP	ΔH	Vm FT.3	Tm INLET	Tm OUTLET	OVEN TEMP.	IMP. OUTLET TEMP.	VACUUM (IN H ₂ O)
A1	4.27		225	.71		5.5	379.144	59	58	258	29	2
2			230	.75		5.8	82.5	59	59	262	29	3
3			220	.68		5.2	85.9	64	59	261	29	2
4			222	.66		5.1	89.2	68	59	259	30	2
5			220	.64		4.9	92.5	71	59	260	31	2
6			229	.65		5.0	95.7	73	60	258	30	2
7		-.33	222	.43		3.3	98.9	75	60	259	29	2
8			225	.43		3.3	401.5	76	60	255	30	2
9			227	.51		3.9	404.1	77	61	258	31	2
10			222	.54		4.1	407.0	77	61	258	30	2
11			232	.57		4.4	409.9	79	62	258	30	2
12			231	.56		4.6	413.0	80	62	255	30	2
B1			226	.85		7.0	416.100	71	61	258	29	4
2			223	.85		7.0	19.9	76	63	257	30	4
3			231	.74		6.1	23.7	79	64	257	31	3.5
4			230	.67		5.5	27.2	81	65	256	31	2
5			228	.58		4.7	30.6	82	65	257	30	2
6			227	.47		3.8	33.7	83	66	255	31	2
7			226	.44		3.6	36.6	83	66	258	31	2
8			228	.34		2.8	39.3	83	67	257	31	2
9			220	.35		2.8	41.7	81	67	256	31	2
10			229	.38		3.1	44.1	82	67	254	30	2
11			223	.34		2.8	46.7	81	67	253	31	2
12			221	.27		2.2	49.1	81	68	254	30	2
							451.2741					
AV							172.1301					

PARTICULATE FIELD DATA

PLANT: LP
DATE: 1-19-94
REPETITION: 3

LOCATION: RTO South E - FORM. TRAIN

OPERATOR:
STACK #: 6X
SAMPLE BOX #: 9
METER BOX #: 7
AMBIENT TEMPERATURE: 40°
BAROMETRIC PRESSURE: 30.5
ASSUMED MOISTURE: 6%
PROBE LENGTH: 11'
NOZZLE DIAMETER: .33033
STACK DIAMETER: 84.5"
METER H: 1.6782
C FACTOR: .84
METER CO-EFFICIENT: .97853

IMPINGERS

	Initial	Final
#1: 100 mls	> DNPH	146
#2: 100 mls		141
#3: —		14
#4: 200 g - SG		220.2
#5:		121.20

COMMENTS:

CO₂ 0%
O₂ 21.0%

FILTER TARE: N/A
PRE-TEST LEAK CHECK

Meter: 0.00 Cu. ft. 15 in. HG
Pitots: 1.80 in. H2O

POST-TEST LEAK CHECK

Meter: 0.018 Cu. ft. 9 in. HG
Pitots: 1.80 in. H2O

≡	⊖	STATIC PRES.	Ts OF	ΔP	√ΔP	ΔH	Vm FT.3	Tm INLET	Tm OUTLET	OVEN TEMP	IMP OUTLET TEMP	VACUUM (IN H ₂ O)
A1	6110		227	.74		6.1	451.721	59	59	253	29	4
2			223	.71		5.8	55.2	54	56	257	29	4
3			227	.71		5.8	58.7	55	56	255	29	4
4			218	.73		6.0	62.2	55	55	256	29	4
5	736		222	.62		5.1	65.7	55	55	253	29	4
6			220	.65		5.3	68.4	55	55	254	29	4
7			224	.46		3.7	72.3	54	54	254	30	4
8			228	.44		4.0	75.1	54	54	257	30	4
9			224	.55		4.5	78.0	53	53	258	30	4
10			223	.62		5.1	81.0	58	53	259	29	5
11			225	.64		5.2	84.3	58	53	256	29	5
12			226	.57		4.7	87.6	58	53	259	29	5
B1			228	.92		7.5	400.723	52	50	258	29	8
2			232	.95		7.8	44.6	59	50	260	27	9
3			224	.81		6.6	48.7	50	50	259	27	8
4			230	.68		5.6	502.4	50	50	260	27	7
5			230	.56		4.6	505.8	50	50	258	29	5
6			221	.52		4.2	508.9	50	49	257	28	5
7			222	.38		3.1	511.8	54	49	258	28	5
8			224	.39		3.2	514.4	55	49	260	29	5
9			225	.37		3.0	516.9	57	49	258	29	5
10			223	.35		2.8	519.5	58	49	257	30	5
11			225	.33		2.7	524.9	58	49	258	30	5
12			227	.35		2.8	524.3	58	49	257	30	5
	7110						526.786					
AV							75.0351					

APPENDIX D

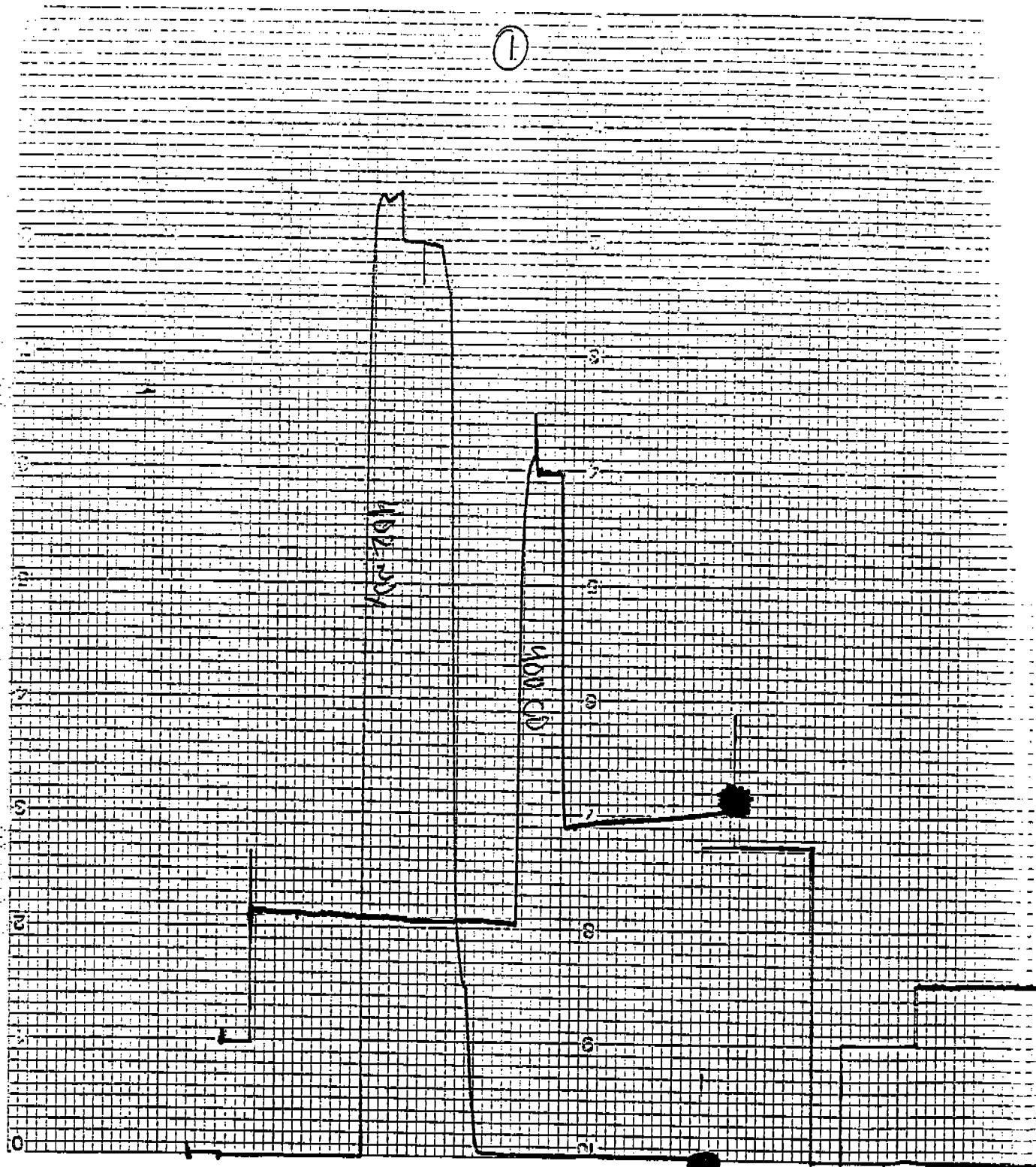
LP 1-18-94
SOUTH PTO EXHAUST

Run 1
(11:15-12:18)

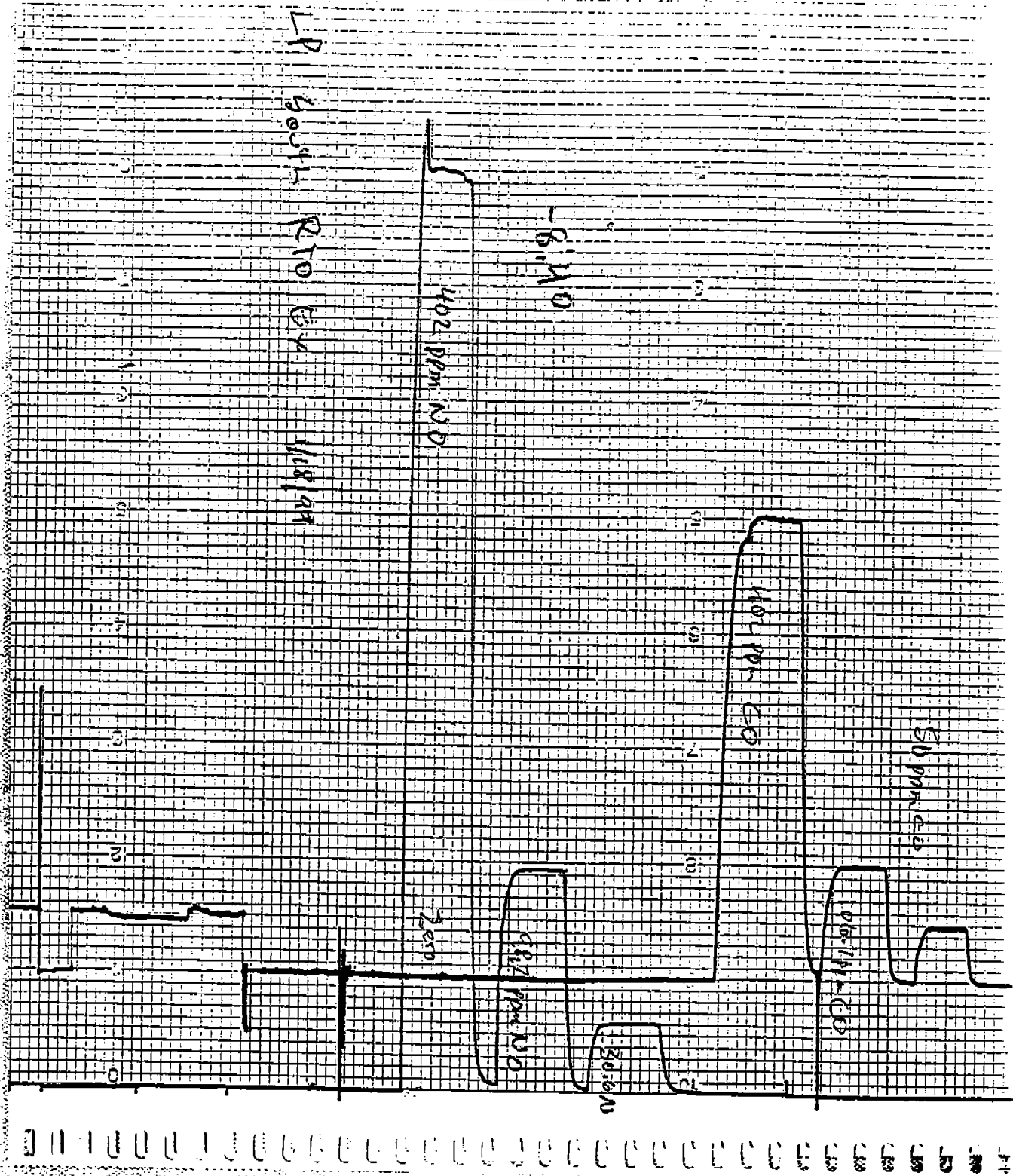
Run 2
(2:58-3:59)

Run 3
(4:55-5:55)

	NOX	CO		NOX	CO		NOX	CO
	5	0		6	0		3	0
	5.5	0		6			3.5	
	5	.2		6.5			4	
	5	.2		6			3.5	
	5.5	0		6			3.5	
	5	.2		6			3.5	
	6	.2		5.5			3.5	
	6	0		5.5			4.5	
	5.5	0		5.5			4.5	
10	6	.2		6			5	
	6	.2		6			5	
	6	.2		5.5			5	
	6	.2		6			5	
	6	0		6			5	
	6	.2		6			5	
	6	.2		6			5	
	6	.2		5.5			5	
	6	.2		5.5			5	
	6	.2		6			5	
20	6	0		5.5			5	
	6	0		5.5			5	
	6	.2		5			5	
	6	0		5.5			5	
	6	0		5			5.5	
	6	0		5			5	
	6	0		5			5.5	
	6	0		5			5	
	6	0		5			5	
	6	0		5.5			5.5	
30	6	0		5			5.5	
	6	0		5.62	0		5.5	0
	5.82	0.09					4.71	
PPM/UNIT	5025	10.05		5.1			503	
PPM	29.245	0.9045		28.662	MD		23.69	MD
				30				



2



③

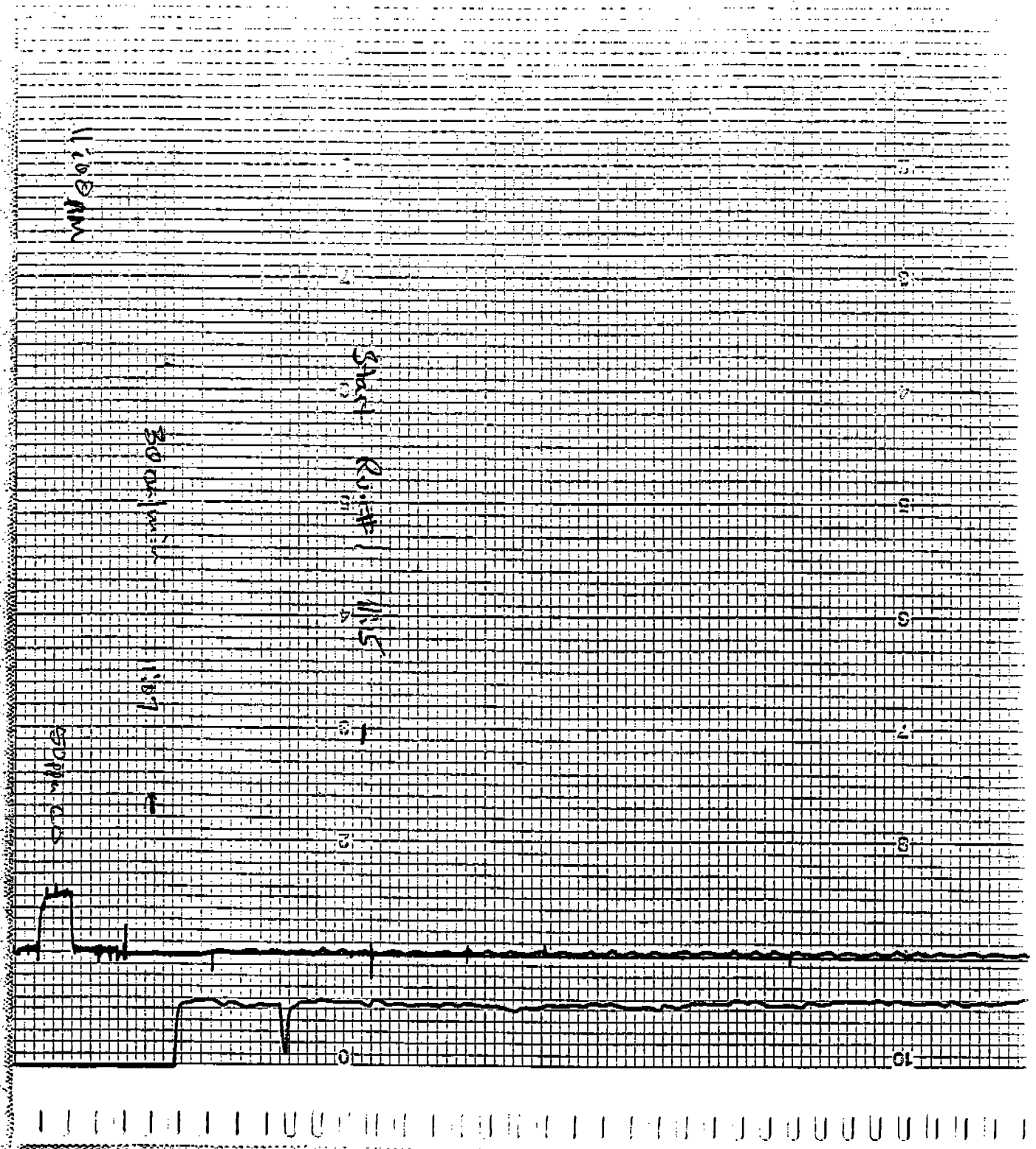
10:53 AM

402 PM NOK

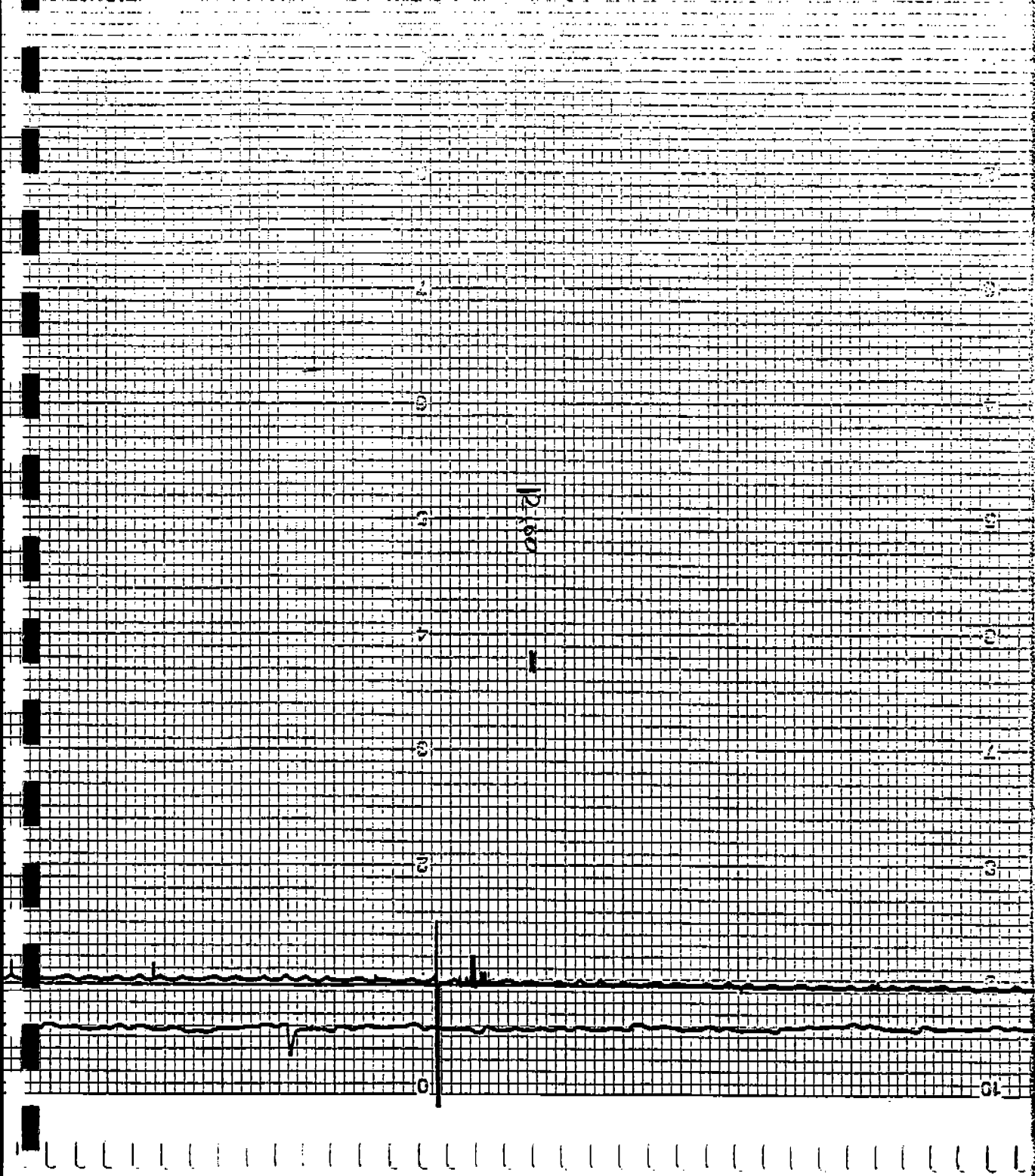
106.700

106.700x

(4)



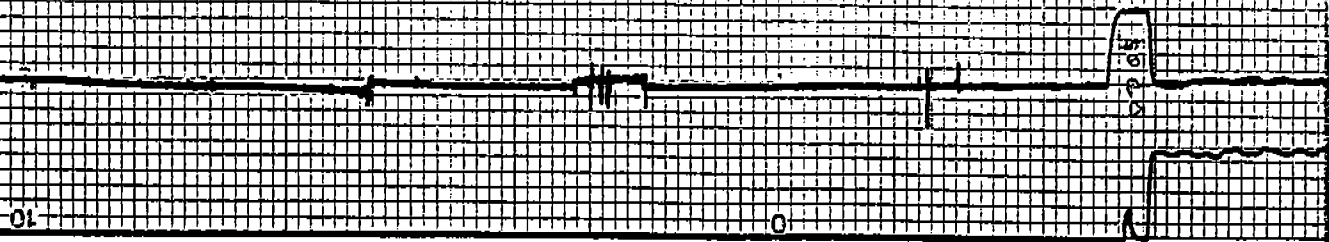
6



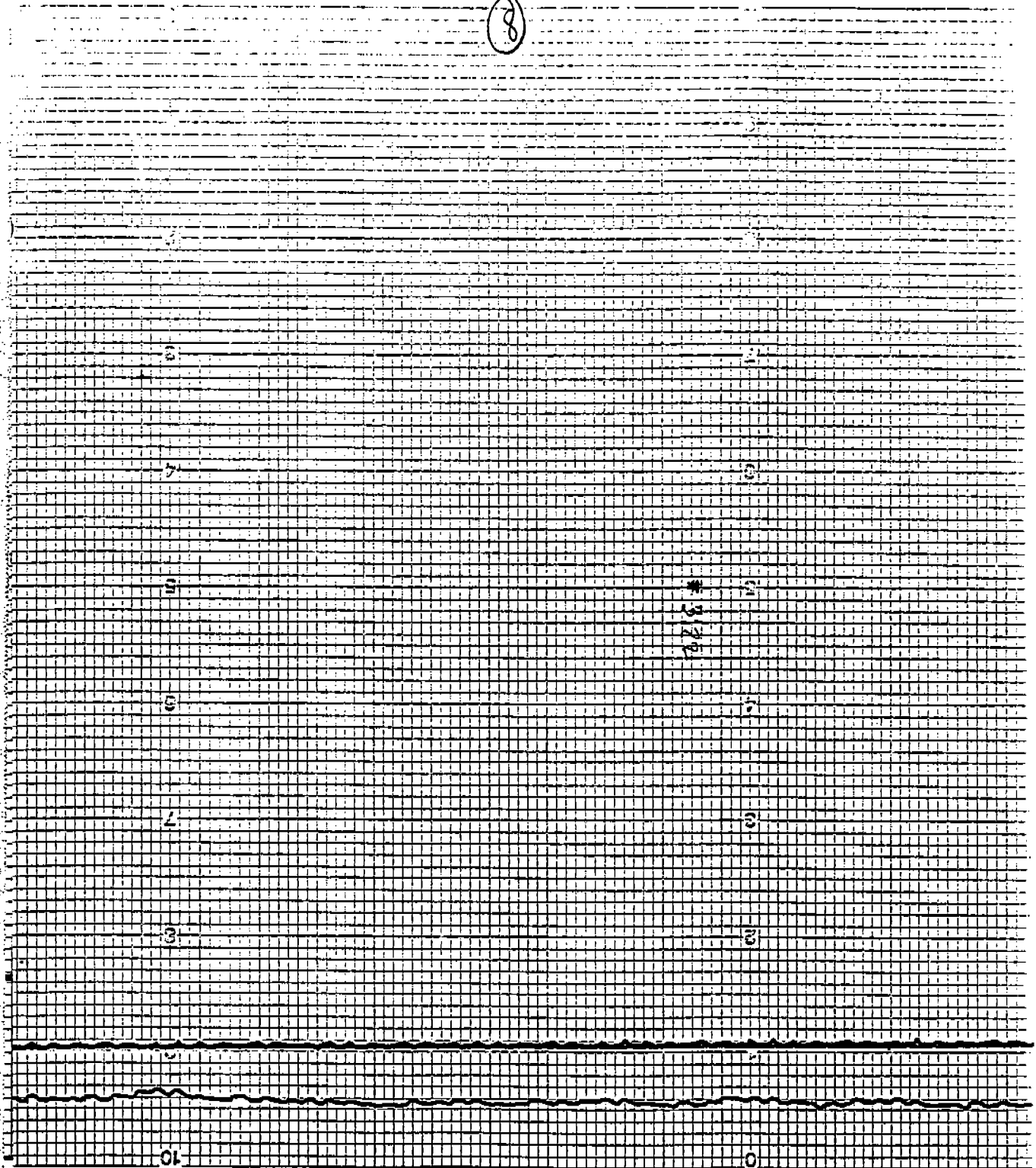
①

RTO South by STAPET Row 2 2.158

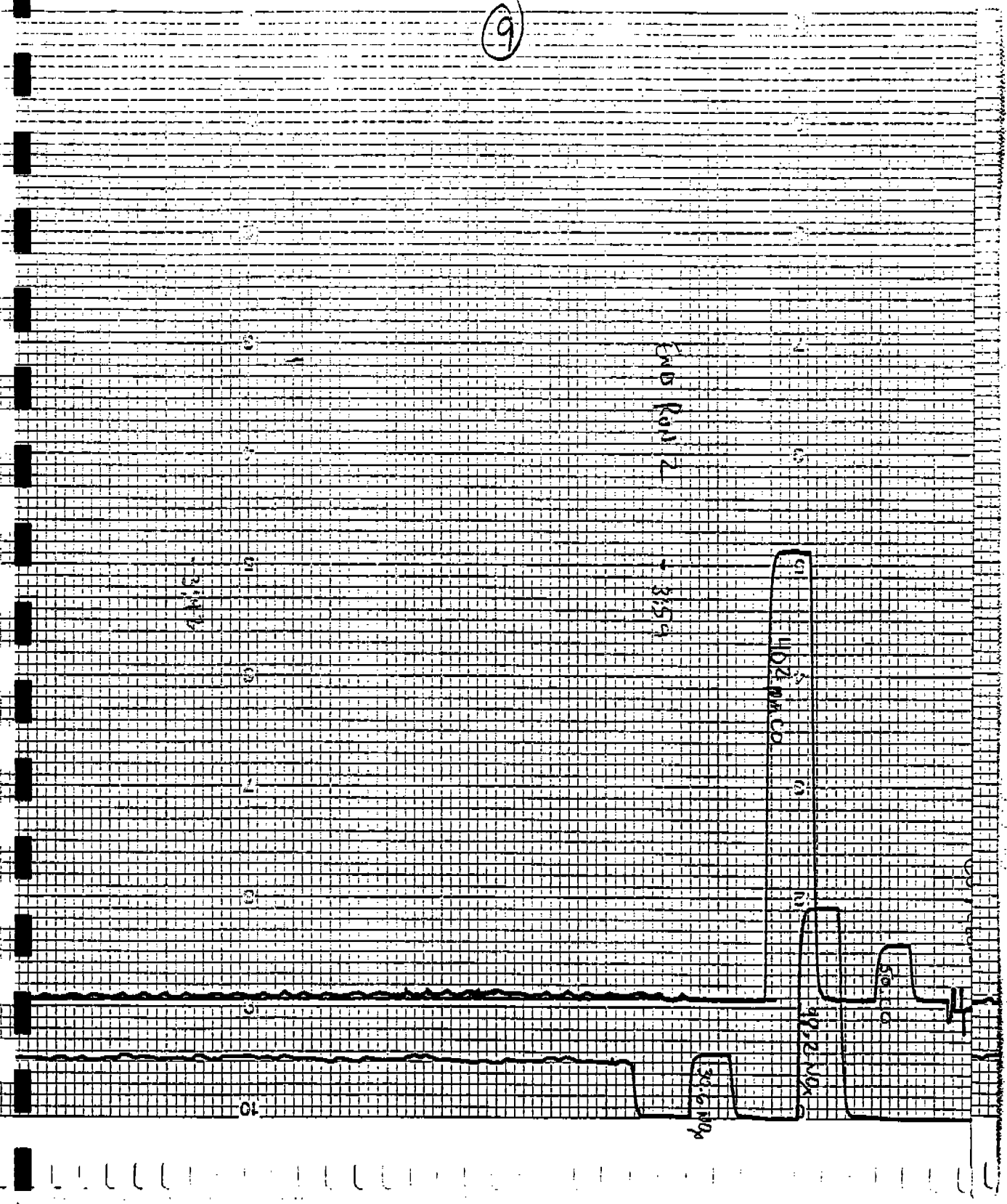
2.155



8



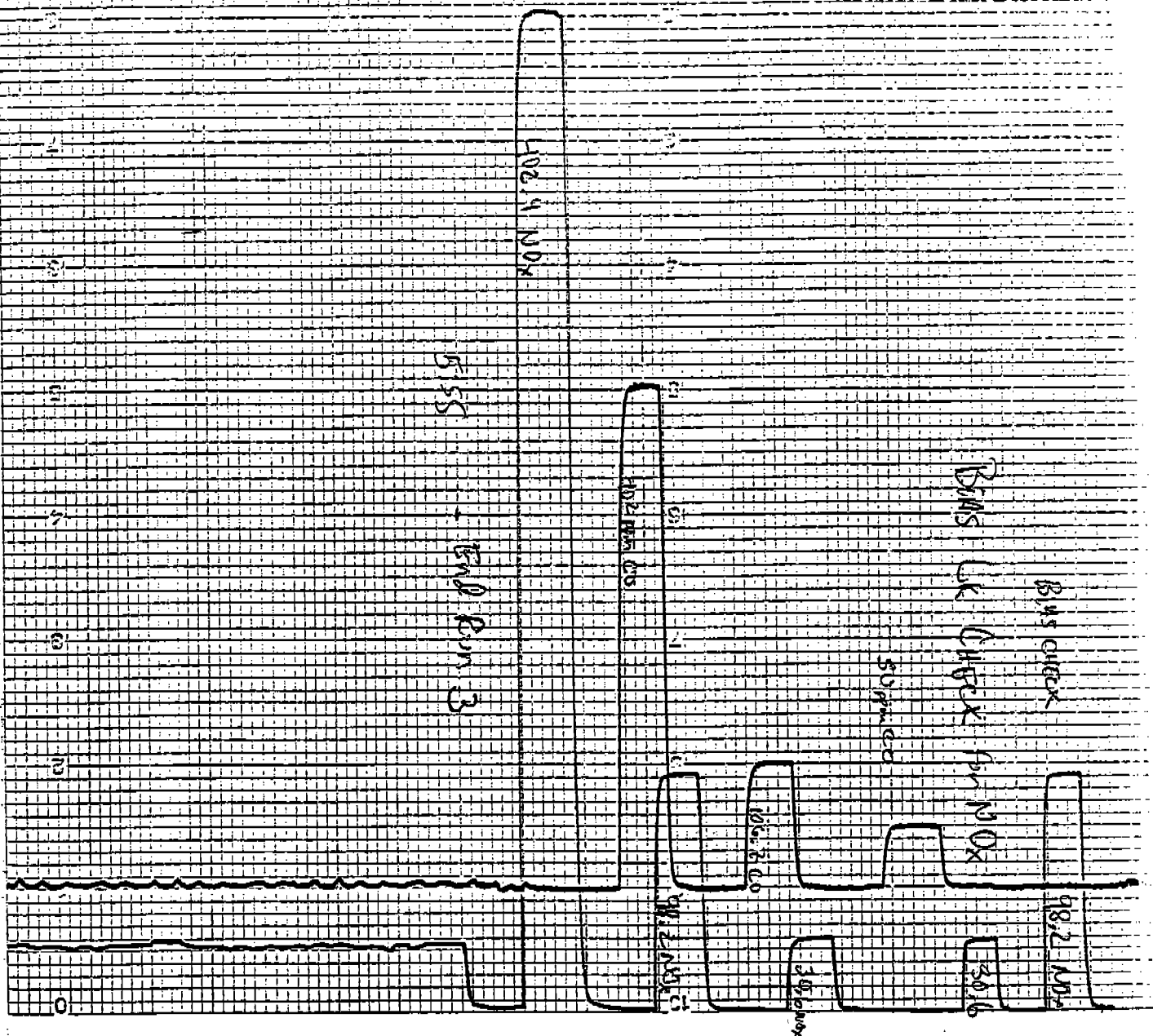
(9)



⑪

67
68
69
70

12



LP 1-19-94
 IZTO SOUTH EXHAUST - VOC's

Run 1
 11:05-11:27 / 2:34-3:14

Run 2
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Run 3
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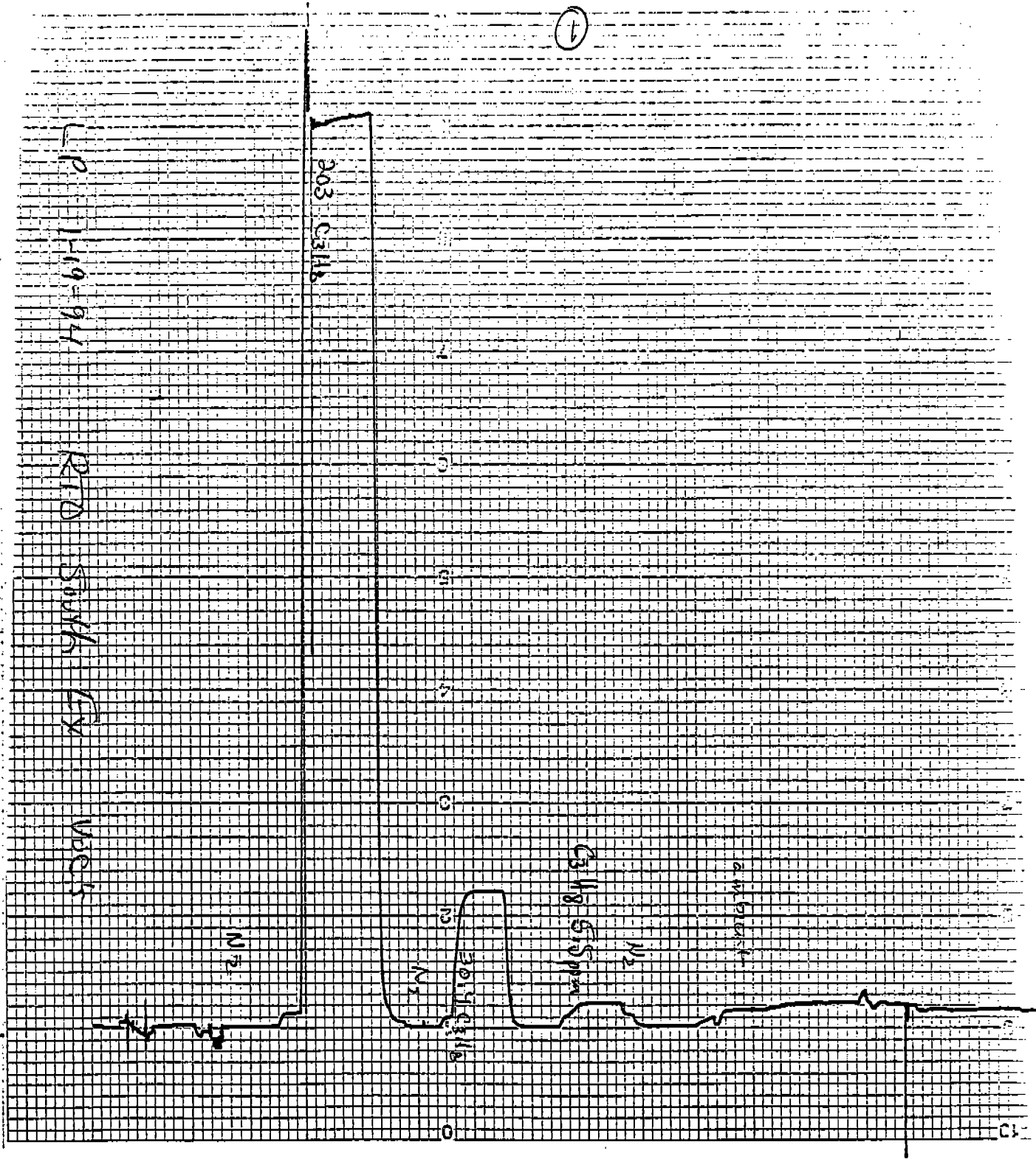
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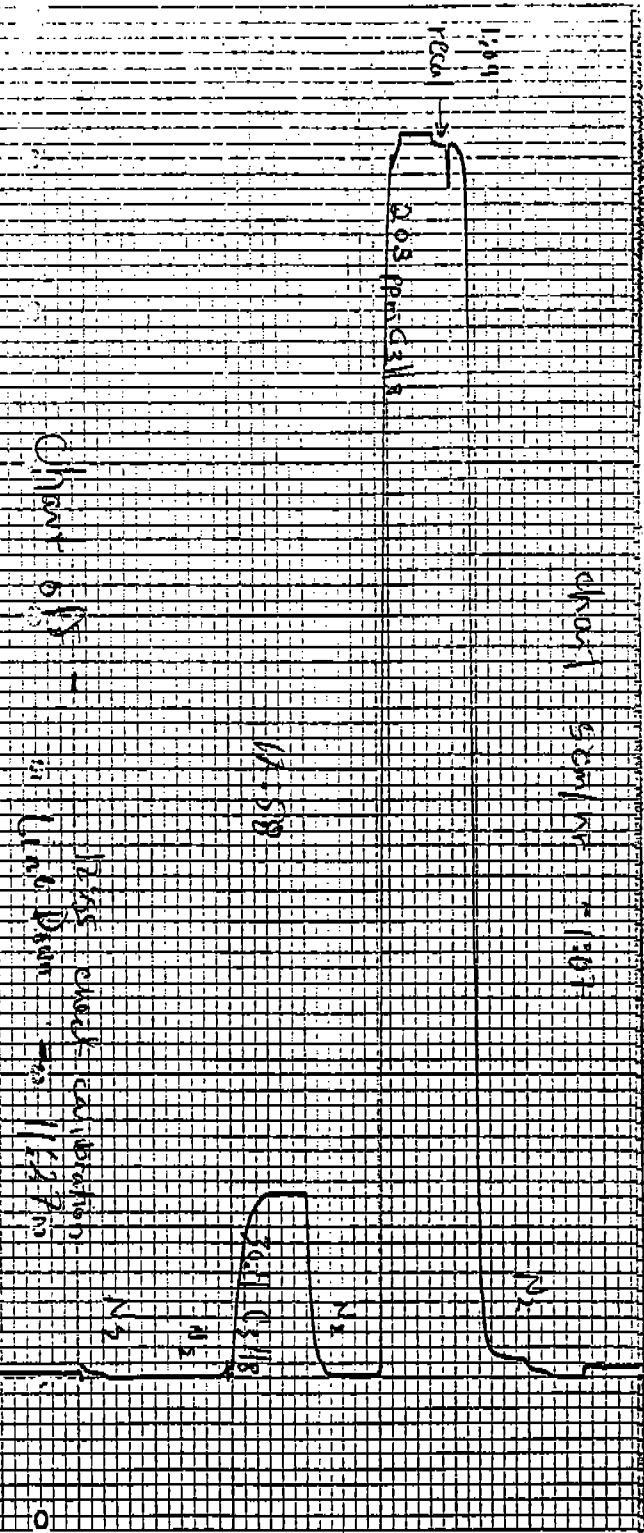
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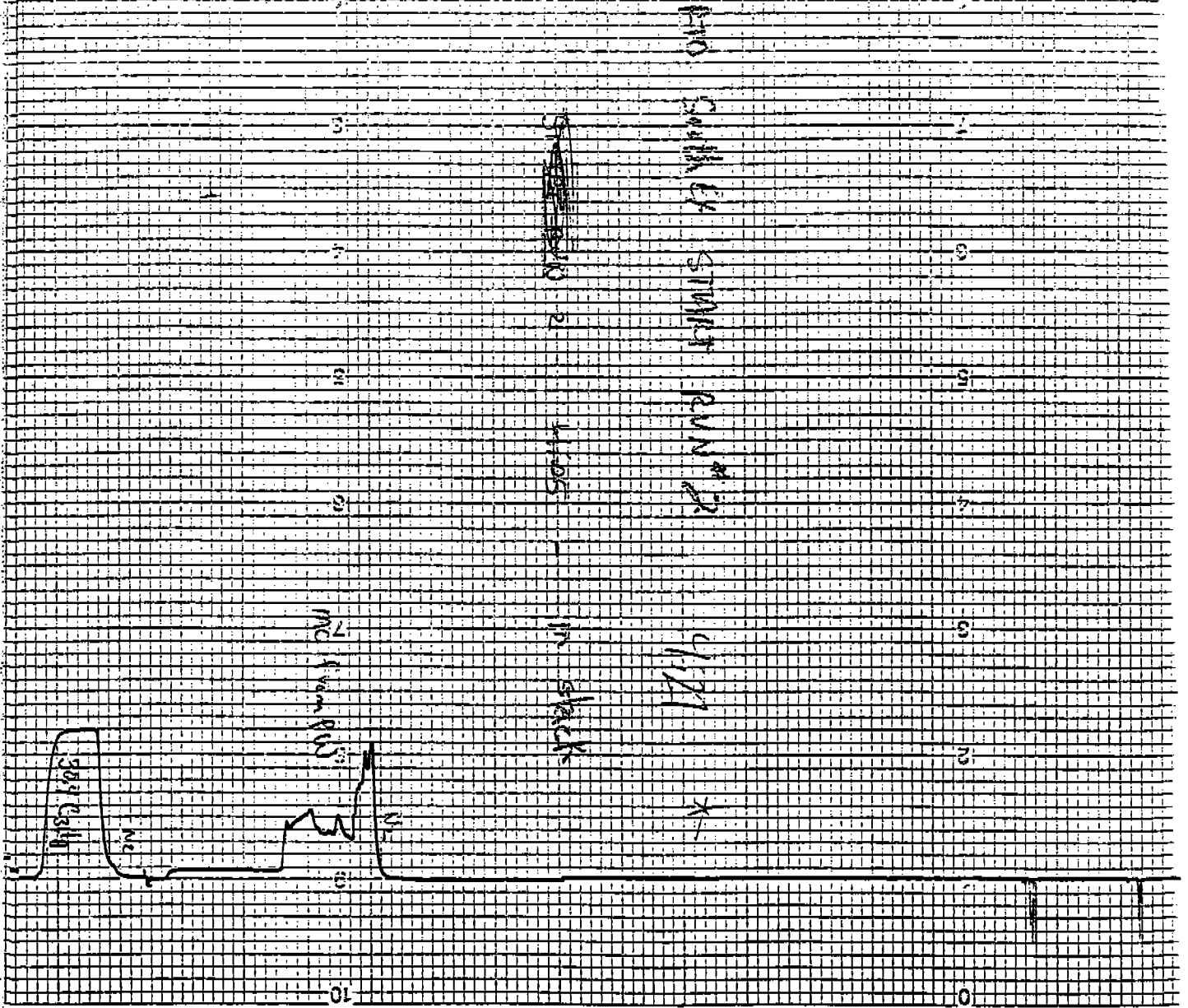
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5.5m C4H8

APPENDIX E

SUMMARY OF PRE METER BOX CALIBRATION

METER BOX NUMBER: 7
CALIBRATION DATE: 1/14/94
CALIBRATED BY: Larry Whicher
BAROMETRIC PRESSURE: 29.83

*
* DELTA H = ORFICE PRESSURE *
* VW = VOLUME OF WET GAS METER *
* TW = AVERAGED TEMPERATURE OF WET METER *
* VD = VOLUME OF DRY GAS METER *
* TD = AVERAGED TEMPERATURE OF DRY GAS METER *
* TIME = DURATION OF EACH POINT RUN *
*

POINT 1
DELTA H = .5 VW = 5 TW = 68
VD = 5.017 TD = 64.8 TIME = 12.02 TEST METER Y = .9804
METER BOX Y = .9699607
METER BOX H = 1.631244

POINT 2
DELTA H = 1 VW = 5 TW = 68
VD = 5.017 TD = 68 TIME = 8.55 TEST METER Y = .9804
METER BOX Y = .9746754
METER BOX H = 1.640711

POINT 3
DELTA H = 1.5 VW = 10 TW = 68
VD = 10.05 TD = 71.8 TIME = 14.41 TEST METER Y = .9804
METER BOX Y = .9789236
METER BOX H = 1.735181

POINT 4
DELTA H = 2 VW = 10 TW = 68
VD = 10.075 TD = 74.5 TIME = 12.29 TEST METER Y = .9804
METER BOX Y = .9802488
METER BOX H = 1.674403

POINT 5
DELTA H = 3 VW = 10 TW = 68
VD = 10.05 TD = 76.5 TIME = 10.09 TEST METER Y = .9804
METER BOX Y = .9839505
METER BOX H = 1.686583

POINT 6
DELTA H = 4 VW = 10 TW = 68
VD = 10.04 TD = 77 TIME = 8.78 TEST METER Y = .9804
METER BOX Y = .9834422
METER BOX H = 1.701173

AVERAGE Y = .9785335
AVERAGE H = 1.678216

Meter Box Calibration

Dry Gas Meter #: 7
 Calibrated by: Larry Whitham
 Date: 1-14-97
 Barometric Pressure: 29.83

Orifice ΔH	Test Meter Volume V_w	Dry Gas Meter Volume V_d	Temoperature				Time e	γ	ΔH_{θ}
			Test Meter. T_w	Dry Gas Meter					
				Inlet T_{di}	Outlet T_{do}	Ave T_d			
55.00	5.000	5.017	68.0	63 72	63 61	64.8	12.02	.9804	
7.00	5.000	5.017	68.0	64 79	63 64	68.0	8.55	.9804	
11.50	10.000	10.050	68.0	70 84	65 68	71.8	14.41	.9804	
12.00	10.000	10.075	68.0	75 85	68 70	74.5	12.29	.9804	
3.00	10.000	10.050	68.0	77 86	71 72	76.5	10.09	.9804	
14.00	10.000	10.040	68.0	77 87	72 72	77.0	8.78	.9804	

$$\gamma = \frac{V_w P_{\text{bar}} (T_d + 460)}{V_d (P_{\text{bar}} + \frac{\Delta H}{13.6}) (T_w + 460)}$$

$$\Delta H_{\theta} = \frac{0.0317 \Delta H}{P_{\text{bar}} (T_d + 460)} \left[\frac{(T_w + 460) \theta}{V_w} \right]^2$$

P_{bar} = Barometric Pressure

DATE: 1-14-94

Poor 29.83

ΔH	V_w	T_w	V_D	T_{D1}	T_{D2}	ΔT_D	S
5 (5 ft ³)	986.000	68	141.508	63	63		
	981.000	68	136.491	72	61		
	5.000	68	5.017		64.8		12.02
10 (5 ft ³)	991.000	68	146.525	66	63		
	986.000	68	141.508	79	64		
	5.000	68	5.017		68.0		8.55
15 (10 ft ³)	1001.000	68	156.575	70	65		
	991.000	68	146.525	84	68		
	10.000	68	10.050		71.8		14.41
20 (10 ft ³)	11.000	68	166.650	75	68		
	1.000	68	156.575	85	70		
	10.000	68	10.075		74.5		12.29
25 (10 ft ³)	21.000	68	176.700	77	71		
	11.000	68	166.650	86	72		
	10.000	68	10.050		76.5		10.09
30 (10 ft ³)	31.000	68	186.740	77	72		
	21.000	68	176.700	87	72		
	10.000	68	10.040		77.0		8.78

SUMMARY OF POST METER BOX CALIBRATION

METER BOX NUMBER : 7
CALIBRATION DATE: 01/20/94
CALIBRATED BY: Dan Barrera
BAROMETRIC PRESSURE (inch Hg): 30.15

*
* DELTA H = ORFICE PRESSURE *
* VW = VOLUME OF WET GAS METER *
* TW = AVERAGED TEEMPERATURE OF WET METER *
* VD = VOLUME OF DRY GAS METER *
* TD = AVERAGED TEMPERATURE OF DRY GAS METER *
* TIME = DURATION OF EACH POINT RUN *
*

POINT 1

DELTA H = 1 VW = 10 TW = 64.5
VD = 9.738 TD = 47.75 TIME = 16.74 TEST METER Y = .9804
METER BOX Y = .9722549
METER BOX H = 1.596335

POINT 2

DELTA H = 1 VW = 10 TW = 65
VD = 9.844 TD = 57 TIME = 16.99 TEST METER Y = .9804
METER BOX Y = .9783744
METER BOX H = 1.618031

POINT 3

DELTA H = 1 VW = 10 TW = 65.5
VD = 9.929 TD = 63.25 TIME = 17.06 TEST METER Y = .9804
METER BOX Y = .980791
METER BOX H = 1.614976

AVERAGE Y = .9771401
AVERAGE H = 1.609781

Post-Test
Meter Box Calibration

Dry Gas Meter #: 7

Calibrated by: *DAN BARRERA*

Date: *1-20-94*

Barometric Pressure: *30.15*

Orifice ΔH	Test Meter Volume V_w	Dry Gas Meter Volume V_d	Temperature			Time θ	γ	$\Delta H @$
			Test Meter T_w	Dry Gas Meter Inlet T_{di}	Outlet T_{do}	Ave T_d		
<i>1.0</i>	<i>10</i>	<i>9.738</i>	<i>64.5</i>	<i>41</i> <i>66</i>	<i>40</i> <i>44</i>	<i>47.25</i>	<i>16:74</i>	<i>.9804</i>
<i>1.0</i>	<i>10</i>	<i>9.844</i>	<i>65</i>	<i>55</i> <i>74</i>	<i>46</i> <i>53</i>	<i>57</i>	<i>16:29</i>	<i>.9804</i>
<i>1.0</i>	<i>10</i>	<i>9.929</i>	<i>65.5</i>	<i>62</i> <i>78</i>	<i>54</i> <i>59</i>	<i>63.25</i>	<i>17:06</i>	<i>.9804</i>

$$\gamma = \frac{V_w P_{\text{bar}} (T_d + 460)}{V_d (P_{\text{bar}} + \frac{\Delta H}{13.6}) (T_w + 460)}$$

$$\Delta H @ = \frac{0.0317 \Delta H}{P_{\text{bar}} (T_d + 460)} \left[\frac{(T_w + 460) \theta}{V_w} \right]^2$$

P_{bar} = Barometric Pressure

ARMSTRONG ENVIRONMENTAL, INC

DRY GAS METER #: 7

DATE: 1-20-94

ΔH	VW	TW	VD	TDT	TDO	ΔTD	θ
1.0 (10FT ³)	191.0	64/64	536.804	41	40		
	181.0	65/65	527.066	66	44		
	10	64.5	9.738		$\rightarrow$	47.75	16:74
1.0 (10FT ³)	201.0	65/65	546.648	55	46		
	191.0	65/65	536.804	74	53		
	10	65	9.844		$\rightarrow$	57	16:99
1.0 (10FT ³)	211.0	65/65	556.577	62	54		
	201.0	66/66	546.648	78	59		
	10	65.5	9.929		$\rightarrow$	63.25	17:06

NATIONAL
42-383

Hg BAROMETER

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PITOT TUBE INSPECTION DATA SHEET

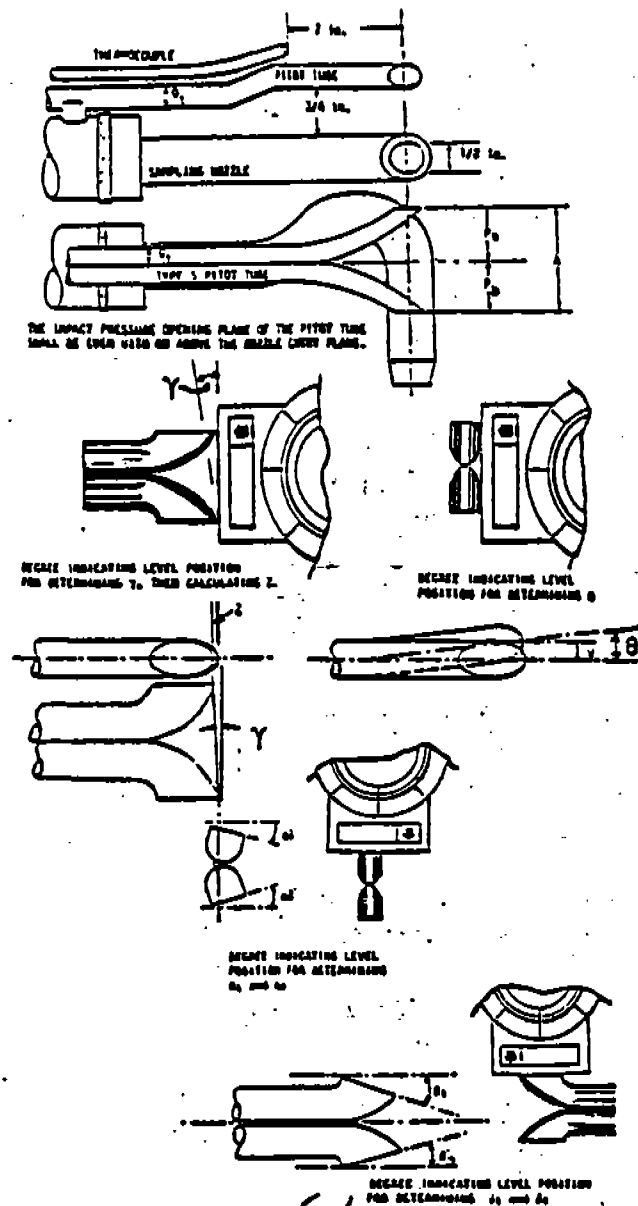
Company Name: _____

Pre-sample

Post Sample

Date 1-11-94

Date _____



yes	level?	
NO	obstructions?	
NO	damaged?	
4°	$-10^\circ < \alpha_1 < +10^\circ$	
4°	$-10^\circ < \alpha_2 < +10^\circ$	
40	$-5^\circ < \beta_1 < +5^\circ$	
30	$-5^\circ < \beta_2 < +5^\circ$	
2°	γ	
1°	θ	
.559	A	
.1281	$1.05 D_t < P_a < 1.5 D_t$	
.278	$1.05 D_t < P_b < 1.5 D_t$	
.465	$3/16" \leq D_t \leq 3/8"$	
.0195	$A \tan \gamma < 0.125"$	
.0097	$A \tan \theta < 0.03125"$	
.003	$P_a = P_b \pm 0.063"$	

Comments:

Glass Lined

Pitot tube/probe number 11-G meets or exceeds all specifications criteria and/or applicable design features* and is hereby assigned a pitot tube calibration factor of 0.84.

Signature

Date

Code [Signature]
1-11-94

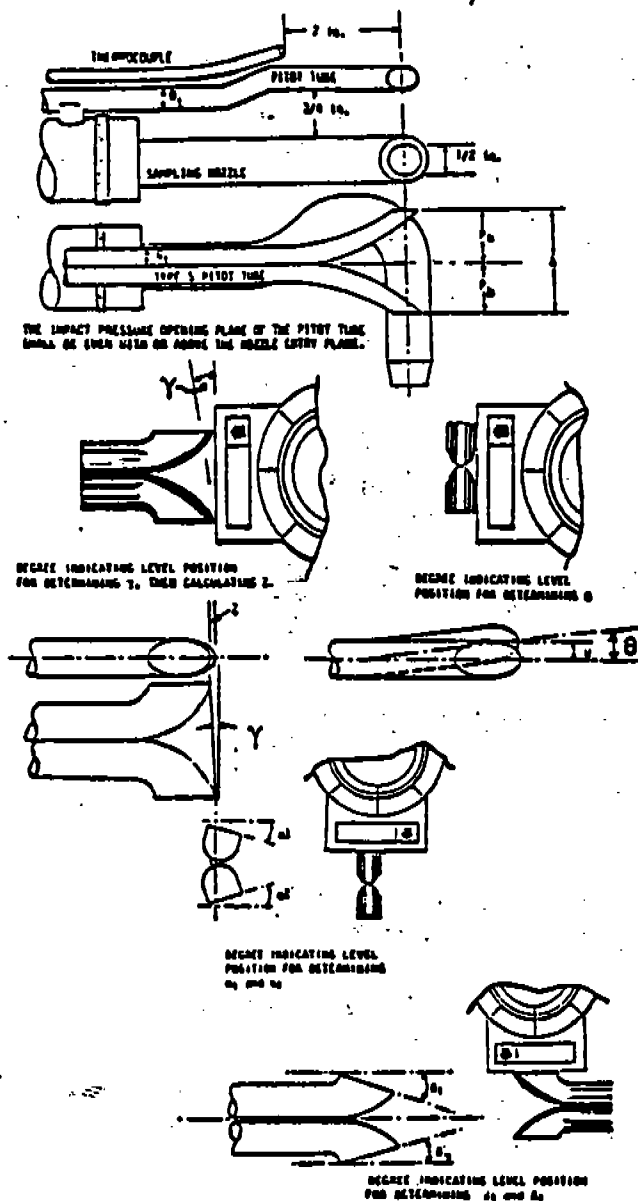
*See 40 CFR 60, Vol. 42, No. 160, Method 2. Verify the minimum 2 inch setback of the thermocouple and the minimum 3/4 inch separation between the pitot tube and the nozzle as shown at the top of this page.

PITOT TUBE INSPECTION DATA SHEET

Company Name: Armstrong

Pre-sample Date 2-1-94

Post Sample Date _____



✓	level?	
NO	obstructions?	
NO	damaged?	
3	$-10^\circ < \alpha_1 < +10^\circ$	
3	$-10^\circ < \alpha_2 < +10^\circ$	
1	$-5^\circ < \beta_1 < +5^\circ$	
1	$-5^\circ < \beta_2 < +5^\circ$	
2	γ	
0	θ	
.621	A	
.309	$1.05 D_t < P_a < 1.5 D_t$	
.312	$1.05 D_t < P_b < 1.5 D_t$	
✓	$3/16" \leq D_t \leq 3/8"$	
.0216	$A \tan \gamma < 0.125"$	
0.0	$A \tan \theta < 0.03125"$	
.003	$P_a = P_b \pm 0.063"$	

Comments: _____

Pitot tube/probe number 1-55 meets or exceeds all specifications criteria and/or applicable design features* and is hereby assigned a pitot tube calibration factor of 0.84.

Signature [Signature]

Date 2-1-94

*See 40 CFR 60, Vol. 42, No. 160, Method 2. Verify the minimum 2 inch setback of the thermocouple and the minimum 3/4 inch separation between the pitot tube and the nozzle as shown at the top of this page.

APPENDIX F

AIR PRODUCTS AND CHEMICALS, INC.
3415 BANNING STREET
DALLAS, TX 75233
FT. WORTH CUSTOMERS CALL
1-800-453-APCI
TELEPHONE (214) 929-1335

DATE: 03/10/93
TIME: 15:49
PAGE: 1

* CERTIFICATE OF ANALYSIS *

ARMSTRONG ENVIRONMENTAL
4747 IRVING BLVD. #201
DALLAS TX 75247

CUSTOMER ACCOUNT : R7812
CUSTOMER ORDER NO : TA93-1233
ORDER NO : 36A-000243
ORDER DETAIL SEQ : 3
SHIPPER NUMBER : 360-3-22144

REMARKS : GAS MIXTURE(S) LISTED BELOW ARE TRACEABLE TO NIST CLASS 5
WEIGHTS AND/OR NIST GAS MIXTURE STANDARD REFERENCE MATERIALS
(SRM's) - REFERENCE APCI 560 FIELD DIRECTIVE BOOK 1 PART A-3.

CERTIFIED GAS MIXTURE: CARBON MONOXIDE IN NITROGEN

BATCH NO	ANALYSIS DATE	BAR CODE	CYLINDER NO	COMPONENT REQUESTED	CONCENTRATION REQUESTED	ANALYTICAL RESULT	UNIT MEASURED
04500	04/08/93	BUY706	3691147738AL	CARBON MONOXIDE Nitrogen	400	402.0 BALANCE	MOLAR

CERTIFICATION

THIS ANALYSIS HAS BEEN PERFORMED UTILIZING APPROVED
ANALYTICAL METHOD(S) AND IS CORRECT TO WITHIN THE
ANALYTICAL ACCURACIES OF THIS (THESE) METHOD(S).

Lisa Overman

AUTHORIZED SIGNATURE

03-20-1993 14:23
Air Products And Chemicals, Inc.
Specialty Gases
10202 Strang Road
LaPorte, Texas 77571
(713) 478-3100

F.002
AIR
PRODUCTS

ANALYTICAL REPORT

SAMPLE OF: Carbon Monoxide in Nitrogen

DATE: 1/11/93

PAGE: 1 of 1

SHIPPER NO.: 865-s-91341 CUSTOMER ORDER NO.: ---

SAMPLE DATE: 1/11/93

REQUESTED BY: Armstrong

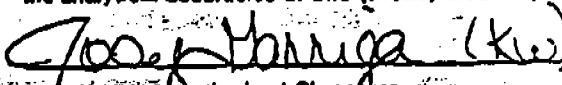
REMARKS:

ANALYSIS

<u>LAB NO.</u>	<u>CYL NO.</u>	<u>COMPONENT REQUESTED</u>	<u>CONCENTRATION REQUESTED</u>	<u>ANALYTICAL RESULT</u>	<u>UNIT OF MEASURE</u>
865-04028	SG9114521BAL	Nitrogen	99.9900		Percent
		Carbon Monoxide	100.00	106.7	Molar PP

CERTIFICATION

This analysis has been performed utilizing the analytical method(s) stated and is correct to within the analytical accuracies of this (these) method(s).

64

Authorized Signature

AIR PRODUCTS AND CHEMICALS, INC.
3415 BANNING STREET
DALLAS, TX 75233
F1. WORTH CUSTOMERS CALL
1-800-453-APCI
TELEPHONE (214) 929-8825

DATE: 05/12/93
TIME: 15:18
PAGE: 1

* CERTIFICATE OF ANALYSIS *

ARMSTRONG ENVIRONMENTAL
4747 IRVING BLVD. #204
DALLAS TX 75247

CUSTOMER ACCOUNT : R7818
CUSTOMER ORDER NO : TA93-1233
ORDER NO : 36A-000243
ORDER DETAIL SEQ : 1
SHIPPER NUMBER : 360-9-22144

REMARKS : GAS MIXTURE(S) LISTED BELOW ARE TRACEABLE TO NIST CLASS S
WEIGHTS AND/OR NIST GAS MIXTURE STANDARD REFERENCE MATERIALS
(SRM's) - REFERENCE APCI 960 FIELD DIRECTIVE BOOK I PART A-3.

PRIMARY GAS MIXTURE : CARBON MONOXIDE IN NITROGEN

BATCH NO	ANALYSIS DATE	BAR CODE	CYLINDER NO	COMPONENT REQUESTED	CONCENTRATION REQUESTED	ANALYTICAL RESULT	UNIT MEASU
04495	04/08/93	BGP203	961094N8	CARBON MONOXIDE Nitrogen	50	50.0 BALANCE	MOLAR

CERTIFICATION

THIS ANALYSIS HAS BEEN PERFORMED UTILIZING APPROVED
ANALYTICAL METHOD(S) AND IS CORRECT TO WITHIN THE
ANALYTICAL ACCURACIES OF THIS (THESE) METHOD(S).

Lisa Overman

AUTHORIZED SIGNATURE



Scott Specialty Gases, Inc.

1290 COMBERMERE STREET, TROY, MI 48063

(313) 589-2950 FAX: (313) 589-2134

CERTIFICATE OF ANALYSIS: EPA PROTOCOL GAS

Customer
ARMSTRONG ENVIROMENTAL
7715 SOVEREIGN ROW
DALLAS TX 75247-9004

Assay Laboratory
Scott Specialty Gases, Inc.
1290 Combermere
Troy, MI 48083

Purchase Order 1317
Scott Project # 556803

ANALYTICAL INFORMATION

Certified to exceed the minimum specifications of EPA Protocol 1 Procedure # G1, Section Number 3.0.4

Cylinder Number ALM037096
Cylinder Pressure 1900 psig

Certification Date 10-11-93
Previous Certification Dates None

General Exp. Date 10-11-95
Acid Rain Exp. 10-11-95
Date

ANALYZED CYLINDER

Components
Nitric Oxide

Certified Concentration
402.4 ppm

Analytical Uncertainty*
±1% NIST Directly Traceable

Total Oxides of Nitrogen
Balance Gas: Nitrogen

402.9 ppm

Reference Value Only

*Analytical uncertainty is inclusive of usual known error sources which at least includes reference standard error & precision of the measurement processes.

REFERENCE STANDARD

Type Expiration Date
NTRM 1687 7-23-95

Cylinder Number
ALM-022382

Concentration
951 PPM NO IN NITROGEN

INSTRUMENTATION

Instrument/Model/Serial #
NO: Beckman/951A/270-082899B

Last Date Calibrated
9-8-93

Analytical Principle
Chemiluminescence

ANALYZER READINGS (Z=Zero Gas R=Reference Gas T=Test Gas r=Correlation Coefficient)

Components	First Triad Analysis	Second Triad Analysis	Calibration Curve
Nitric Oxide	Date: 10-4-93 Response Units: mv Z1=0.00 R1=95.10 T1=40.30 R2=95.10 Z2=0.00 T2=40.30 Z3=0.00 T3=40.30 R3=95.10 Avg. Conc. of Cust. Cyl. 402.9 ppm	Date: 10-11-95 Response Units: mv Z1=0.00 R1=95.10 T1=40.20 R2=95.10 Z2=0.00 T2=40.20 Z3=0.00 T3=40.20 R3=95.10 Avg. Conc. of Cust. Cyl. 401.9 ppm	Concentration=A+Bx+Cx²+Dx³+Ex⁴ r=0.99999 NTRM1687 Constants: A=0.1377292 B=10.00145 C=0 D=0 E=0
			Concentration=A+Bx+Cx²+Dx³+Ex⁴
			Concentration=A+Bx+Cx²+Dx³+Ex⁴

Special Notes

If this product is used for Acid Rain Rule Compliance, the Acid Rain Expiration Date noted above applies per 40 CFR Part 75, Appendix H. Otherwise, the General Expiration Date applies.

Air Products and Chemicals, Inc.
SPECIALTY GAS DEPARTMENT
12722 S. WENTWORTH AVENUE
CHICAGO, IL 60628

Certificate of Analysis - EPA Protocol #1 Gases

Page 1 of 1

PERFORMED ACCORDING TO SECTION 3.0.4 (Procedure #G1)
Certified Accuracy 1% NIST Traceable

Customer:

APCI
3415 BANNING ST
DALLAS, TX. TX 75233

Notes:

Order No: 855-016677-01
Batch No: 861-11964

Cylinder No: SG91134688AM.
Cylinder Pressure: 2000 psig
Certification Date: 04/26/93
Expiration Date: 04/26/95

PO: Rel:

***** Reference Standards ***** Analytical Instrumentation *****
Standard Instrument Make/Model Serial Last Measurement
Concentration Number
94.0000 PPM Rosemount 951a 0101877 04/08/93 CHEMILUMINESCENCE

***** Certified Concentration ***
Cylinder # Concentration
SG9103337BAL 98.2 PPM

Component

Nitric Oxide

Balance Gas: Nitrogen

Analytical Data*

Component: Nitric Oxide

First Analysis Date: 04/15/93

Zero	Test Gas	*** Ref. Gas ***
39.9	98.3	98.2
39.9	98.2	98.2
39.9	98.4	98.2
Average:	98.3	

Second Analysis Date: 04/26/93

Zero	Test Gas	*** Ref. Gas ***
39.7	98.2	98.2
39.7	98.2	98.2
39.7	98.2	98.2
Average:	98.2	

*** Calculations performed per Section 3.0.4 subsection 4.1.7

Analyst:

Richard VanDyke
Richard VanDyke

Approved By:

Robert McNear
Robert McNear



Scott Specialty Gases, Inc.

1290 COMBERMERE STREET, TROY, MI 48083

(313) 589-2950 FAX: (313) 589-2134

CERTIFICATE OF ANALYSIS: EPA PROTOCOL GAS

Customer
ARMSTRONG ENVIROMENTAL
7715 SOVEREIGN ROW
DALLAS TX 75247-9004

Assay Laboratory
Scott Specialty Gases, Inc.
1290 Combermere
Troy, MI 48083

Purchase Order 1317
Scott Project # 556803

ANALYTICAL INFORMATION

Certified to exceed the minimum specifications of EPA Protocol 1 Procedure # G1, Section Number 3.0.4

Cylinder Number AAL18218
Cylinder Pressure 1900 psig

Certification Date 10-11-93
Previous Certification Dates None

General Exp. Date 10-11-95
Acid Rain Exp. 10-11-95
Date

ANALYZED CYLINDER

Components
Nitric Oxide

Certified Concentration
30.60 ppm

Analytical Uncertainty*
±1% NIST Directly Traceable

Total Oxides of Nitrogen
Balance Gas: Nitrogen

31.00 ppm

Reference Value Only

*Analytical uncertainty is inclusive of usual known error sources which at least includes reference standard error & precision of the measurement processes.

REFERENCE STANDARD

Type Expiration Date
CRM 1684 9-17-94

Cylinder Number
ALM-024698

Concentration
95.6 PPM NO IN N₂

INSTRUMENTATION

Instrument/Model/Serial #
NO: Horiba/OPE-235/483814

Last Date Calibrated
9-13-93

Analytical Principle
Chemiluminescence

ANALYZER READINGS (Z=Zero Gas R=Reference Gas T=Test Gas r=Correlation Coefficient)

Components

First Triad Analysis

Second Triad Analysis

Calibration Curve

Nitric Oxide

Date: 10-4-93 Response Units: mv
Z1=0.00 R1=95.60 T1=30.60
R2=95.60 Z2=0.00 T2=30.60
Z3=0.00 T3=30.60 R3=95.60
Avg. Conc. of Cust. Cyl. 30.60 ppm

Date: 10-11-93 Response Units: mv
Z1=0.00 R1=95.60 T1=30.60
R2=95.60 Z2=0.00 T2=30.60
Z3=0.00 T3=30.60 R3=95.60
Avg. Conc. of Cust. Cyl. 30.60 ppm

Concentration=A+Bx+Cx²+Dx³+Ex⁴
r=0.99999 SRM 1684B
Constants: A=-0.000967584
B=1.000115 C=0
D=0 E=0

Concentration=A+Bx+Cx²+Dx³+Ex⁴

Concentration=A+Bx+Cx²+Dx³+Ex⁴

Special Notes

If this product is used for Acid Rain Rule Compliance, the Acid Rain Expiration Date noted above applies per 40 CFR Part 75, Appendix H. Otherwise, the General Expiration Date applies.

68

Analyst Frank P. Doran

AIR PRODUCTS
4822 INDUSTRY LANE
DURHAM, NC 27713

CERTIFICATE OF ANALYSIS-EPA PROTOCOL MIXTURES

REFERENCE #: 88-23473 CYLINDER #:SG9113690 CYL PRESSURE:2000PSIG

EXPIRATION DATE:4-7-96

LAST ANALYSIS DATE: 4-7-93

BATCH# 05867

CUSTOMER: AIR PRODUCTS
DALLAS, TX 75233

P.O.#

METHOD: EPA PROTOCOL # 1 3.0.4. G-1

STANDARD:

SRM #: 2644

CYL #: FF39583

CONC.: 244.5 PPM

VALID DATE:7-13-90

EXPIR. DATE:7-18-94

INSTRUMENT:

COMPONENT: BECKMAN THC

MODEL #: 400

SERIAL #: 1003052

LAST CAL: 4-2-93

COMP: C3H8
MEAN CONC: 203 PPM

REPLICATE CONC.

DATE: 4-7-93

DATE:

203 PPM

203 PPM

204 PPM

COMP:
MEAN CONC:

REPLICATE CONC.

DATE:

DATE:

COMP:
MEAN CONC:

REPLICATE CONC.

DATE:

DATE:

BALANCE GAS: NITROGEN

REPLICATE DATA

DATE: 4-7-93

Z	0	R	425	C	352.9
R	426	Z	0	C	353.7
Z	0	C	354.6	R	425

REPLICATE DATA

DATE:

Z		R		C
R		Z		C
Z		C		R

REPLICATE DATA

DATE:

Z		R		C
R		Z		C
Z		C		R

COMPONENT:C3H8

DATE:

Z		R		C
R		Z		C
Z		C		R

COMPONENT:

DATE:

Z		R		C
R		Z		C
Z		C		R

COMPONENT:

DATE:

Z		R		C
R		Z		C
Z		C		R

Z=ZERO C=CANDIDATE R=REFERENCE

ANALYST:

APPROVED BY:

"THIS REPORT STATED ACCURATELY THE RESULTS OF THE INVESTIGATION MADE UPON THE MATERIAL SUBMITTED TO THE ANALYTICAL LABORATORY. EVERY EFFORT HAS BEEN MADE TO DETERMINE OBJECTIVELY, THE INFORMATION REQUESTED; HOWEVER, IN CONNECTION WITH ITS RENDERING OF THIS REPORT, AIR PRODUCTS SHALL HAVE NO LIABILITY IN EXCESS OF ITS ESTABLISHED CHARGE FOR THE SERVICE. ANY USE OF THIS REPORT OR THE INFORMATION CONTAINED HEREIN SHALL BE AT THE SOLE RISK OF THE USER."

AIR PRODUCTS
4822 INDUSTRY LANE
DURHAM, NC 27713

CERTIFICATE OF ANALYSIS-EPA PROTOCOL MIXTURES

REFERENCE #: 88-23475 CYLINDER #:SG9113687 CYL PRESSURE:2000PSIG

EXPIRATION DATE:10-7-94

LAST ANALYSIS DATE: 4-7-93

BATCH# 05866

CUSTOMER: AIR PRODUCTS
DALLAS TX. 75233

P.O.#

METHOD: EPA PROTOCOL # 1 3.0.4. G-1

STANDARD:

SRM #: 2643

CYL #: FF39574

CONC.: 101 PPM

VALID DATE:1-26-93

EXPIR. DATE:1-26-97

INSTRUMENT:

COMPONENT: BECKMAN THC

MODEL #: 400

SERIAL #: 1003052

LAST CAL: 4-2-93

COMP: C3H8

MEAN CONC: 30.4 PPM

REPLICATE CONC.

DATE: 4-7-93

DATE:

30.4 PPM

30.5 PPM

— 30.4 PPM

COMP:

MEAN CONC:

REPLICATE CONC.

DATE:

DATE:

COMP:

MEAN CONC:

REPLICATE CONC.

DATE:

DATE:

BALANCE GAS: NITROGEN

REPLICATE DATA

DATE: 4-7-93

Z	0	R	547	C	164.6
R	548	Z	0	C	165.5
Z	0	C	164.9	R	548

REPLICATE DATA

DATE:

Z	R	C
R	Z	C
Z	C	R

REPLICATE DATA

DATE:

Z	R	C
R	Z	C
Z	C	R

COMPONENT:C3H8

DATE:

Z	R	C
R	Z	C
Z	C	R

COMPONENT:

DATE:

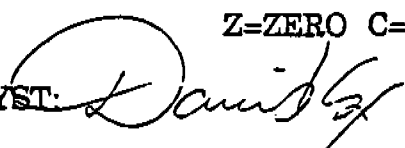
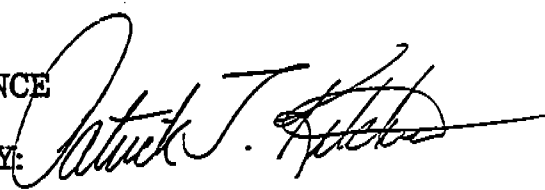
Z	R	C
R	Z	C
Z	C	R

COMPONENT:

DATE:

Z	R	C
R	Z	C
Z	C	R

Z=ZERO C=CANDIDATE R=REFERENCE

ANALYST: APPROVED BY: 

"THIS REPORT STATED ACCURATELY THE RESULTS OF THE INVESTIGATION MADE UPON THE MATERIAL SUBMITTED TO THE ANALYTICAL LABORATORY. EVERY EFFORT HAS BEEN MADE TO DETERMINE OBJECTIVELY, THE INFORMATION REQUESTED; HOWEVER, IN CONNECTION WITH ITS RENDERING OF THIS REPORT, AIR PRODUCTS SHALL HAVE NO LIABILITY IN EXCESS OF ITS ESTABLISHED CHARGE FOR THE SERVICE. ANY USE OF THIS REPORT OR THE INFORMATION CONTAINED HEREIN SHALL BE AT THE SOLE RISK OF THE USER."

AIR PRODUCTS AND CHEMICALS, INC.
SPECIALTY GAS DEPARTMENT
10202 STRANG ROAD
LA PORTE, TX 77571
TELEPHONE (713) 478-3100
FAX (713) 478-3112

DATE: 01/25/93
TIME: 10:17
PAGE: 1

* CERTIFICATE OF ANALYSIS *

ARMSTRONG ENVIRONMENTAL
4747 IRVING BLVD. #204
DALLAS TX 75247

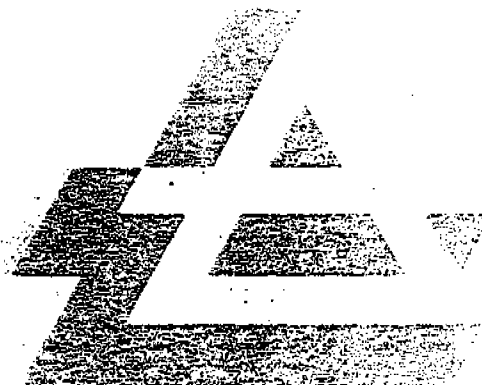
CUSTOMER ACCOUNT : R7818
CUSTOMER ORDER NO : TA93-1233
ORDER NO : 360-037684
ORDER DETAIL SEQ : 1

REMARKS : GAS MIXTURE(S) LISTED BELOW ARE TRACEABLE TO NIST CLASS S
WEIGHTS AND/OR NIST GAS MIXTURE STANDARD REFERENCE MATERIALS
(SRM's) - REFERENCE APCI SGD FIELD DIRECTIVE BOOK I PART A-3.

** ANALYSIS **

CERTIFIED GAS MIXTURE: PROPANE IN NITROGEN

BATCH NO	ANALYSIS DATE	SAR CODE	CYLINDER NO	COMPONENT REQUESTED	CONCENTRATION REQUESTED	ANALYTICAL RESULT	UNIT OF MEASURE
04133	01/25/93	BMB383	SG040625AS	PROPANE Nitrogen	5	5.5 BALANCE	MOLAR PPM



CERTIFICATION

THIS ANALYSIS HAS BEEN PERFORMED UTILIZING APPROVED
ANALYTICAL METHOD(S) AND IS CORRECT TO WITHIN THE
ANALYTICAL ACCURACIES OF THIS (THESE) METHOD(S).

Jose Arruga
AUTHORIZED SIGNATURE

APPENDIX F.

**PRODUCTION SUMMARY
(LOUISIANA PACIFIC)**

1b/msf 3/4

URANIA MDF STACK TEST OPERATIONAL SUMMARY

01/18/94

	DRYER 1	DRYER 2
Dry Furnish Moisture	9.3 - 11.2%	10.2 - 12.8%
Inlet Temperature	171- 221 ⁰ F	174 - 196 ⁰ F
Outlet Temperature	115 - 130 ⁰ F	115 - 131 ⁰ F

CONTINUOUS PRESS

Resin Usage (U-F)	10.4 gal/min.
Wax Usage (Emulsion)	0.5 gal/min.
Line Speed	39.5 ft/min.
Press Temperature	387 - 396 ⁰ F
Thickness	0.307 in ³
Density	55.8 lbs/cu.ft.

PRODUCTION

30,133 lbs/hr.

*Nominal thickness = 0.25 inch (1/4)

$$\frac{1 \text{ hr}}{\text{hr}} \times \frac{\text{ft}^3}{\text{ft}^3} = \frac{\text{ft}^3}{\text{hr}} \times \frac{1}{\text{ft}} = \frac{\text{ft}^2}{\text{hr}} \times \frac{1}{1000} = \frac{\text{msf}}{\text{hr}} (0.307)$$

$$\frac{\text{msf}}{\text{hr}} (0.307) \times \frac{0.307}{0.75} = 0.409$$

$$\frac{30133}{55.8} \times \frac{12}{0.307} \times 0.409 = 8.63 \frac{\text{msf}}{\text{hr}} \quad 3/4$$

URANIA MDF STACK TEST OPERATIONAL SUMMARY

01/19/94

	DRYER 1	DRYER 2
Dry Furnish Moisture	8.6 - 12.3%	10.6 - 13.2%
Inlet Temperature	144- 215 ⁰ F	174 - 206 ⁰ F
Outlet Temperature	114 - 129 ⁰ F	116 - 130 ⁰ F

CONTINUOUS PRESS

Resin Usage (U-F)	9.0 - 10.5 gal/min.
Wax Usage (Emulsion)	0.5 gal/min.
Line Speed	38.0 - 44.1 ft/min.
Press Temperature	378 - 398 ⁰ F
Thickness	0.272 - 0.306 in.*
Density	52.9 - 55.8 lbs/cu.ft. 54.35

PRODUCTION

25,671 - 31,768 lbs/hr.

28719.5

*Nominal thickness = 0.25 inch (1/4)

$$\frac{28719.5}{54.35} \times \frac{12}{0.289} \times \frac{0.289}{0.75} = 8.454 \frac{\text{hr}}{\text{hr}} \frac{3}{4}$$

1000

URANIA MDF STACK TEST OPERATIONAL SUMMARY

01/20/94

	DRYER 1	DRYER 2
Dry Furnish Moisture	8.8 - 10.5%	8.3 - 11.7%
Inlet Temperature	169 - 215 ⁰ F	169 - 185 ⁰ F
Outlet Temperature	120 - 136 ⁰ F	114 - 140 ⁰ F

CONTINUOUS PRESS

Resin Usage (U-F)	11.4 - 11.9 gal/min.
Wax Usage (Emulsion)	0.5 gal/min.
Line Speed	29.0 - 30.0 ft/min.
Press Temperature	387 - 405 ⁰ F
Thickness	0.430 - 0.434 in* 0.432
Density	50.4 - 51.5 lbs/cu.ft. 51.0

PRODUCTION

28,234 - 29,620 lbs/hr.
28927

*Nominal thickness = 0.375 inch (3/8)

$$\frac{28927}{51} \times \frac{12}{.432} \times \frac{.432}{0.75} = 9.08 \text{ mst/hr } 3/4$$

URANIA MDF STACK TEST OPERATIONAL SUMMARY

01/21/94

	DRYER 1	DRYER 2
Dry Furnish Moisture	9.0 - 11.0%	9.1 - 11.6%
Inlet Temperature	182 - 215 ⁰ F	179 - 204 ⁰ F
Outlet Temperature	118 - 133 ⁰ F	116 - 133 ⁰ F

CONTINUOUS PRESS

Resin Usage (U-F)	10.4 - 11.2 gal/min.
Wax Usage (Emulsion)	0.5 gal/min.
Line Speed	44.0 - 43.5 ft/min.
Press Temperature	375 - 407 ⁰ F
Thickness	0.283 - 0.293 in* 0.288
Density	53.4 - 54.1 lbs/cu.ft. 53.8

PRODUCTION

30,001 - 30,267 lbs/hr.

30134

*Nominal thickness = 0.25 inch (1/4)

$$\frac{30134}{53.8} \times \frac{12}{0.75} = 8.96 \text{ mst/hr} \quad 3/4$$