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N. C. DEPT. OF NATURAL
RESOURCES AND
COMMUNITY DEVELOPMENT
FEB 8 1988

DIVISION OF ENVIRONMENTAL
MANAGEMENT

SOURCE SAMPLING
for
PARTICULATE EMISSIONS
PIEDMONT ASPHALT PAVING COMPANY
GOLD HILL, NORTH CAROLINA
February 1 & 2, 1988


Pete Galloway
Piedmont Asphalt Paving


G. Sumner Buck, III
President


Ken Allmendinger
Team Leader

ENVIRONMENTAL CORPORATION

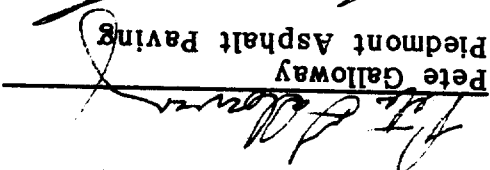
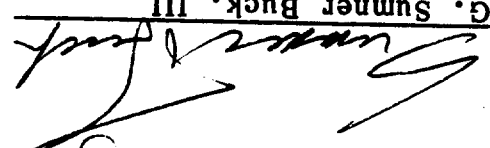
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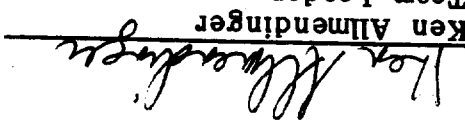
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ENVIRONMENTAL CORPORATION

N. C. DEPT. OF NATURAL
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FEB 3 1988
DIVISION OF ENVIRONMENTAL
MANAGEMENT RECORDS

SOURCE SAMPLING
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February 1 & 2, 1988


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ENVIRONMENTAL CORPORATION

February 5, 1988

Mr. Pete Galloway
Piedmont Asphalt Paving Company
P.O. Box 931
Salisbury, NC 28144

Re: Particulate Emissions Test - Gold Hill North Carolina

Dear Mr. Galloway:

Enclosed you will find four copies of our report on the particulate emissions test we conducted at your plant. Based on our test results, your plant does pass both EPA New Source Performance Standards and those set by the State of North Carolina. Therefore, the plant is operating in compliance with Federal and State Standards.

You will want to sign the report covers and send two copies to:

Mr. Yin-Pong Chang, P.E.
North Carolina DNR
Div. of Environmental Mgmt.
919 N. Main Street
Mooresville, NC 28115

You will need to keep one copy of the report at the plant. We certainly have enjoyed working with you and look forward to serving you again in the future.

Sincerely,

G. Sumner Buck, III
President

GSBIII:kr

Enclosures

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I. INTRODUCTION

On February 1 & 2, 1988, personnel from RAMCON Environmental Corporation (REC) conducted a source emissions test for particulate emissions compliance at Piedmont Asphalt Paving's Astec drum mix asphalt plant located in Gold Hill, North Carolina. RAMCON personnel conducting the test were Ken Allmendinger, Team Leader and Shawn Greenwood. Kim Rea was responsible for the laboratory analysis including taring the beakers and filters and recording final data in the laboratory record books. Custody of the samples was limited to Mr. Allmendinger and Ms. Rea.

The purpose of the test was to determine if the rate of particulate emissions from the plant's baghouse and the total contaminants by weight (grain loading) is below the allowable N.S.P.S. limits set by EPA and the State of North Carolina.

II. TEST RESULTS

Table I summarizes the test results. The grain loading limitation for EPA is .04 gr/DSCF and is specified in 39 FR 9314, March 8, 1974, 60.92 Standards for Particulate Matter (1), as amended. The allowable emissions for the State of North Carolina are the same as those set by EPA.

Mr. Yin-Pong Chang of North Carolina's Department of Natural Resources observed the testing conducted by RAMCON. Shawn Greenwood and Ken Allmendinger conducted the opacity test (Reference Method 9), which ranged from 0% to 20% on all three test runs and therefore, meets N.S.P.S. requirements.

TABLE I

SUMMARY OF TEST RESULTS
February 1 & 2, 1988

Test Run	Time	Grain Loading	Isokinetic Variation	Actual Emissions
1	14:32 to 15:43	0.0467 gr/DSCF	104%	3.9 lbs/hr
2	08:30 to 09:35	0.0224 gr/DSCF	103%	1.8 lbs/hr
3	10:26 to 11:34	0.0457 gr/DSCF	102%	3.5 lbs/hr
Average:		0.0383 gr/DSCF		3.1 lbs/hr

On the basis of these test results, the average grain loading of the three test runs was below the .04 gr/DSCF emissions limitation set by EPA and the State of North Carolina. Therefore, the plant is operating in compliance with Federal and State Standards.

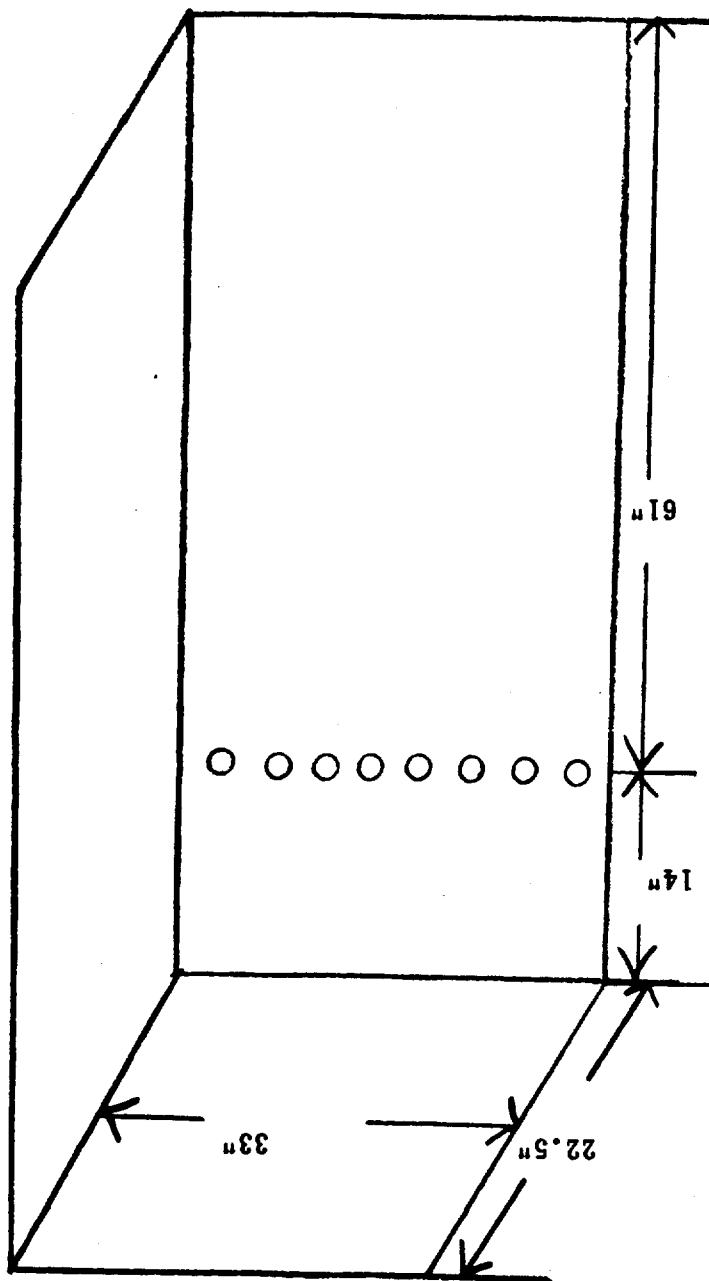
III. TEST PROCEDURES

- A. Method Used: The source sampling was conducted in accordance with requirements of the U.S. Environmental Protection Agency as set forth in 39 FR 9314, March 8, 1974, 60.93, as amended.
- B. Problems Encountered: No problems were encountered that affected testing.

C. Sampling Site: The emissions test was conducted after a baghouse on a rectangular stack measuring 33" x 22.5" with an equivalent diameter of 26.8". Eight sampling ports were placed 14" down (0.52 diameters upstream) from the top of the stack and 61" up (2.3 diameters downstream) from the last flow disturbance. Thirty two points were sampled, four through each port for two minutes each.

Points on a Diameter	Probe Mark
1	*7.8"
2	13.4"
3	19.1"
4	24.7"

*Measurements include a 5.0" standoff.



IV. THE SOURCE

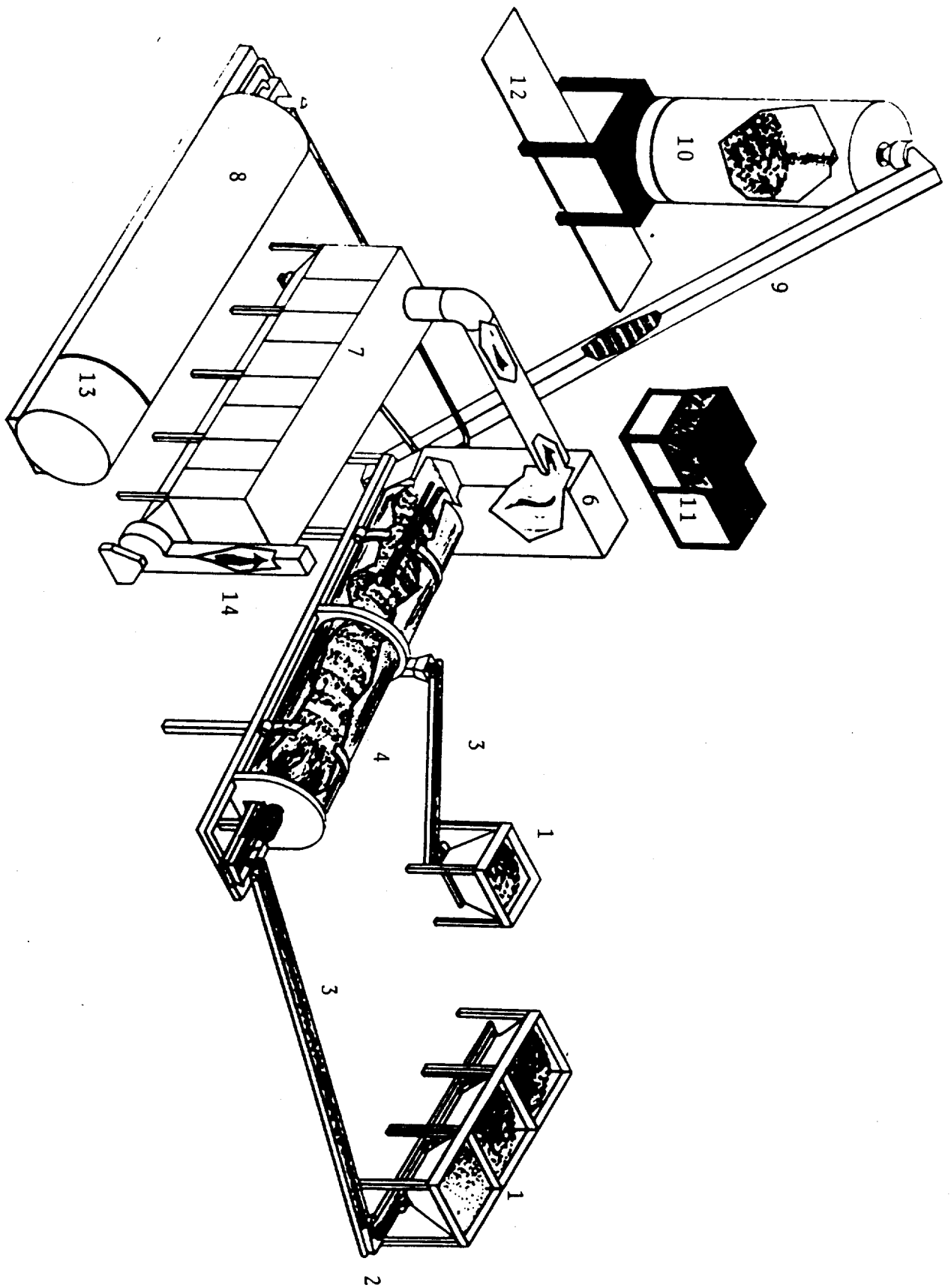
IV. THE SOURCE

(4)

Piedmont Asphalt Paving employs an Astec drum mix asphalt plant which is used to manufacture hot mix asphalt for road pavement. The process consists of blending prescribed portions of cold feed materials (sand, gravel, screenings, chips, etc.) uniformly and adding sufficient hot asphalt oil to bind the mixture together. After the hot asphalt mix is manufactured at the plant, it is transported to the location where it is to be applied. The hot asphalt mix is spread evenly over the surface with a paver and then compacted with a heavy roller to produce the final product.

The following is a general description of the plant's manufacturing process: The cold feed materials (aggregate) are dumped into four separate bins which in turn feed a common continuous conveyor. The aggregate is dispensed from the bins in accordance with the desired formulation onto the cold feed system conveyor to an inclined weigh conveyor then to a rotating drum for continuous mixing and drying at approximately 300°F. The required amount of hot asphalt oil is then injected onto and mixed into the dried aggregate. The now newly formed hot asphalt mix is pulled to the top of a storage silo by conveyor. The hot asphalt mix is then discharged from the storage silo through a slide gate into waiting dump trucks, which transport the material to a final destination for spreading. The rated capacity of the plant will vary with each aggregate mix and moisture content with a 5% surface moisture removal.

The drum mixer uses a burner fired with #2 fuel oil to heat air to dry the aggregate, and the motion of the rotating drum to blend the aggregate and hot asphalt oil thoroughly. The air is drawn into the system via an exhaust fan. After passing through the burner and the mixing drum, the exhaust gasses pass through a baghouse. The baghouse is manufactured by Astec. The exhaust gasses are drawn through the baghouse and discharged to the atmosphere through a stack. The design pressure drop across the tube-sheet is 1 - 6 inches of water. The particulate matter, which is removed by the baghouse, is reinjected into the drum mixer.



ASTEC - DRUM MIX BAGHOUSE

1. Aggregate bins: Virgin aggregate is fed individually into each of four bins by type. It is metered onto a conveyor belt running under the bins to a shaker screen. The proportion of each aggregate type is determined by the job mix formula and pre-set to be metered out to meet these specifications.

2. Preliminary oversize screen: The aggregate is fed through a shaker screen where oversize rocks and foreign material is screened out of the mix.

3. Weigh conveyor belt: The aggregate is conveyed to the rotary drum dryer on a conveyor belt which weighs the material. The production rate is determined by this weight reading.

4. Rotary drum dryer/mixer: The aggregate is fed into the rotary drum dryer where it is tumbled by lighting into a well in front of a flame which drives off the moisture. Further mixing is also accomplished in this drum. Hot liquid asphalt is injected approximately one-third of the way down the inclined drum where it is mixed with the aggregate.

5. Burner: The fuel fired burner is used to provide the flame which dries the aggregate.

6. Knock off baffling: A baffling plate is inserted in the "dirty" side plenum as a knock out for heavy particles in the air stream. These particles fall to the bottom of the baghouse.

7. Baghouse: The hot gases are pulled through the bags into the clean air plenum. The solid particulate matter is trapped on the dust coat buildup on the bags. A bag cleaning cycle consisting of jet burst of air from the inside (or clean air side) of the bags sends a large bubble of air down the inside of the bags shaking loose buildup on the bag surface. This particulate matter is collected at the bottom of the baghouse and reinjected into the drum mixer where it is used as part of the finished project.

8. Liquid asphalt storage: The liquid asphalt is stored in this heated tank until it is needed in the mixer. The amount of asphalt content and its temperature are pre-set for each different type job.

9. Conveyor to surge/storage bin: The finished product of aggregate mixed with liquid asphalt is conveyed to a surge bin.

10. Surge/storage bin: The asphaltic cement is dumped into this surge bin and metered out to dump trucks which pull underneath a slide gate at the bottom of the bin.

11. Control/operators house: The entire plant operation is controlled from this operator's house.

12. Truck loading scale: As the trucks receive the asphalt from the storage/surge bin they are weighed on the loading scale which tells the plant operator the amount of asphalt that is being trucked on each individual load.

13. Fuel Storage

14. Stack

DATA SUMMARY

Plant

1. Manufacturer of plant Astec
2. Designed maximum operating capacity 150 TPH @ 3 % moisture.
3. Actual operation rate 115 TPH @ 5.5 % moisture.
4. Startup date 2-1-88
5. Type of fuel used in dryer #2 fuel
6. Quantity of fuel consumption 1.7 gals/hr

Aggregate

7. Name/type of mix I-2
8. Percent asphalt in mix 690 %
9. Temperature of asphalt 290
10. Sieve/Screening analysis: % Passing:

1"	<u>100</u>	#4	<u>95</u>	#40	<u>21</u>
3/4"	<u>100</u>	#4	<u>77</u>	#80	<u>13</u>
1/2"	<u>98</u>	#8	<u>67</u>	#200	<u>5.8</u>

Baghouse

11. Manufacturer Astec
12. No. of bags 630. Type of bags Monet
13. Air to cloth ratio 5 to 1. Designed ACFM 28000
14. Square feet of bags 5525
15. Type of cleaning: pulse jet ☒ reverse air ☐
16. Plenum pulse ☐ other ☐
17. Cleaning cycle time 10 sec
18. Interval between cleaning cycle 10 sec
19. Pressure drop across baghouse 6 in psi.
19. Pulse pressure on cleaning cycle 110 psi.

COMPANY NAME

Richard Hopcraft Company

DATE

2-1-88

COMPANY REPRESENTATIVE

Pat Hollen

PLANT DATA (8)

COMPANY NAME Bedmont Asphalt paving Corp COMPANY REP. DATE 2/1/88 PHONE # 704-279-8225
PLANT LOCATION Gold Hill N.C.
PLANT MFG. Astec PLANT MODEL # 4 Local PLANT TYPE drum mix
MIX SPECIFICATION # _____ OIL SPECIFICATION # _____

24 Hour Time	Fuel Oil — Nat. Gas — Propane — Coal	Burner Setting	Aggregate TPH	Recycle TPH	Liquid Asphalt TPH	Mix Temp. °F	Inches Water	
							Venturi Pressure Drop	Baghouse
2:20	No. 2	35%	102		4.8	319	4	4
2:35		50%	186.5		5.1	320	4	4
2:47		62%	107.5		5.2	308	4	4
2:57		72%	109		5.2	316	5	5
3:05		75%	111.2		5.3	315	5 1/2	5 1/2
3:15		54%	113.5		5.4	303	5 1/2	5 1/2
3:26		65%	113.6		5.10	290	6	6
3:30		61%	113.9		5.7	310	6	6
3:45		65%	115.8		5.7	295	6	6
3:55		60%	116.0		4.19	255	6	6
4:05		75%	113.7		6.1	280	6	6
4:15		55%	110.1		4.4	279	6 1/2	6 1/2
4:35		55%	101.2		3.8	310	4	4
4:45		60%	103.13		3.9	319	5	5
4:55		65%	105.12		3.9	310	6	6
5:05		65%	103.17		3.9	309	6 1/2	6 1/2
5:15		65%	103.6		5.1	306	7	7
5:25		65%	104.4		4.8	300	7 1/4	7 1/4
5:35		60%	104.5		4.10	295	7 1/2	7 1/2
5:40		70%	104.16		4.10	300	7 1/2	7 1/2
10:40		70%	105.8		4.2	295	8	8
10:50		70%	106.1		4.2	290	9 1/4	9 1/4
11:01		75%	106.13		4.2	285	10 1/2	10 1/2
11:10		78%	110.14		4.2	285	11 1/4	11 1/4
11:20		1/80%			4.2	285	11 1/4	11 1/4

(6)

COMPANY REP.

PLANT LOCATION

PLANT MFG.

PLANT MFG.

MIX SPECIFICATION #

OIL SPECIFICATION

PLANT MODEL # _____ PLANT TYPE _____

-PHONE #

DATE _____

11:30	NO. 2	98%	110.5	14.7	2.10	4.74
11:40						

V. EQUIPMENT USED

EQUIPMENT USED

Equipment used on conducting the particulate emissions test was:

A. The Lear Siegler PM-100 stack sampler with appropriate auxiliary equipment and glassware. The train was set up according to the schematic on the nex page.

B. An Airguide Instruments Model 211-B (uncorrected) aneroid barometer was used to check the barometric pressure.

C. Weston dial thermometers are used to check meter temperatures. An Analogic Model 2572 Digital Thermocouple is used for stack temperatures.

D. A Hays 621 Analyzer was used to measure the oxygen, carbon dioxide and carbon monoxide content of the stack gases. For non-combustion sources, A Bacharach Instrument Company Fyrite is used for the gas analysis.

E. Filters are mady by Schleicher and Schuell and are type I-HV with a porosity of .03 microns.

F. The acetone is reagent grade or ACS grade with a residue of $\leq .001$.

VI. LABORATORY PROCEDURES & RESULTS

LABORATORY PROCEDURES FOR PARTICULATE SAMPLING

(11)

I. Field Preparation

A. FILTERS: Fiberglass 4" sampling filters are prepared as follows:

Filters are removed from their box and numbered on the back side with a felt pen. The numbering system is continuous from job to job. The filters are placed in a dessicator to dry for at least 24 hours. Clean plastic petri dishes, also numbered, top and bottom, are placed in the dessicator with the filters. After dessication, the filters are removed one at a time and weighed on the Sartorius analytical balance, then placed in the correspondingly numbered petri dish. Weights are then recorded in the lab record book. Three filters are used for each complete particulate source emissions test and there should be several extra filters included as spares.

B. SILICA GEL: Silica Gel used for the test is prepared as follows:

Approximately 200 g of silica gel is placed in a wide mouth "Mason" type jar and dried in an oven (175°C for two hours). The open jar are removed and placed in a dessicator until cool (2 hours) and then tightly sealed. The jars are then numbered and weighed on the triple beam balance to the closest tenth of a gram, and this weight is recorded for each sealed jar. The number of silica gel jars used is the same as the number of filters. Silica gel should be indicating type, 6-16 mesh.

II. Post-Testing Lab Analysis

A. FILTERS: The filters are returned to the lab in their sealed glass filter holder which was used in field sampling. In the lab these holders are opened. The filter is placed in its petri dish with the lid off and returned to the dessicator for at least 24 hours. The top half of the filter holder is washed into the corresponding probe wash bottle and the bottom half of the filter holder is washed into the corresponding impinger catch bottle. (See II, C and D). After dessication, the filters are reweighed. The final weight is recorded in the lab record book. The filter pick up weight is calculated and recorded also. This procedure is repeated for all filters used in the field.

Alternately, the test team may opt to oven dry the filters at 220°F for two to three hours, weigh the sample, and use this weight as a final weight.

B. SILICA GEL: The sealed silica gel jars should be reweighed on the triple-beam balance and their weights recorded as shown on previous page.

C. **PROBE RINSINGS:** In all tests, a probe wash-out analysis will be necessary. These samples are returned in sealed Mason jars and consist of A.R. Acetone with an unknown solid content. Clean 250 ml beakers are used to make this analysis. These should be immaculately washed and rinsed with deionized water, then oven dried at 105°C for about one hour. The beakers should be moved to the dessicator to cool for ninety (90) minutes, then labeled with a pencil and weighed on the Sartorius analytical balance. Any variance from this procedure should be duplicated exactly when reweighing, as this procedure has been found to be quite sensitive. After preparing the necessary number of beakers (one for each probe wash and one blank) the Mason jars should be opened, poured into the beaker, and any material remaining on the jar walls rinsed with an acetone wash bottle into the beaker. The amount of liquid in the beaker should be noted on the analysis form. The acetone rinsings are evaporated on a warming plate. The liquid is kept swirled with an air sweep to prevent "bumping". When the acetone is evaporated the beakers are weighed as in Section II A.

D. **IMPINGER CATCH:** In some testing cases, the liquid collected in the impingers must be analyzed for solids content. This involves a similar procedure to the probe wash solids determination, except that the liquid is deionized water.

E. **ACETONE:** Conduct a blank analysis of acetone in the 1 gallon glass container. This acetone will be used in the field for rinsing the probe, nozzle, and top half of the filter holder. Performing such a blank analysis prior to testing will insure that the quality of the acetone to be used will not exceed the .001% residual purity standard.

SPECIAL NOTE

When sampling sources high in moisture content, (such as asphalt plants) the filter paper sometimes sticks to the filter holder. When removing the filter it may tear. In order to maintain control of any small pieces of filter paper which may be easily lost, they are washed with acetone into the probe washing. This makes the filter weight light (sometimes negative) and the probe wash correspondingly heavier. The net weight is the same and no particulate is lost. This laboratory procedure is taught by EPA in the Quality Assurance for Source Emissions Workshop at Research Triangle Park and is approved by EPA.

WEIGHING PROCEDURE - SARTORIUS ANALYTICAL BALANCE

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The Sartorius balance is accurate to 0.1 mg and has a maximum capacity of 200 grams. The balance precision (standard deviation) is 0.05 mg. Before weighing an item, the balance should first be zeroed. This step should be taken before every series of weighings. To do this, the balance should have all weight adjustments at "zero" position. The beam arrest lever (on the lower left hand side toward the rear of the balance) is then slowly pressed downward to full release position. The lighted vernier scale on the front of the cabinet should align the "zero" with the mark on the cabinet. If it is not so aligned, the adjustment knob on the right hand side (near the rear of the cabinet) should be turned carefully until the marks align. Now return the beam arrest to horizontal arrest position. The balance is now "zeroed".

To weigh an item, it is first placed on the pan. And the sliding doors are closed to avoid air current disturbance. The weight adjustment knob on the right hand side must be at "zero". The beam arrest is then slowly turned upward. The lighted scale at the front of the cabinet will now indicate the weight of the item in grams. If the scale goes past the divided area, the item then exceeds 100 g weight (about 3-1/2 ounces) and it is necessary to arrest the balance (beam arrest lever) and move the lever for 100 g weight away from you. It is located on the left hand side of the cabinet near the front, and is the knob closest to the side of the cabinet. The balance will not weigh items greater than 200 grams in mass, and trying to do this might harm the balance. Remember -- this is a delicate precision instrument.

After the beam is arrested, in either weight range, the procedure is the same. When the weight of the item in grams is found, "dial in" that amount with the two knobs on the left hand side (near the 100 g lever) color coded yellow and green. As you dial the weight, the digits will appear on the front of the cabinet. When the proper amount is dialed, carefully move the arrest lever down with a slow, steady turn of the wrist. The lighted dial will appear, and the right hand side knob (front of cabinet) is turned to align the mark with the lower of the two lighted scale divisions which the mark appears between. When these marks are aligned, the two lighted digits along with the two indicated on the right hand window on the cabinet front are the fractional weight in grams (the decimal would appear before the lighted digits) and the whole number of grams weight is the amount "dial in" on the left.

In general, be sure that the beam is in "arrest" position before placing weight on or taking weight off of the pan. Don't "dial in" weight unless the beam is arrested. The balance is sensitive to even a hand on the table near the balance, so be careful and painstaking in every movement while weighing.

Plant Location Redmont Asphalt Sample Location hot mix asphalt plant
 Relative humidity in lab 52 % Density of Acetone (pa) .7858 mg/ml

Blank volume (Va) 200 ml
 Date/Time wt. blank 2/3/88
 Date/Time wt. blank 2/4/88

Gross wt. 154.3742 mg
 Gross wt. 154.3733 mg
 Ave. Gross wt. 154.3738 mg
 Tare wt. 154.3735 mg
 Weight of blank (mab) .0003 mg
 Acetone blank residue concentration (Ca) = (mab) / (Va) (pa) = (.000049 mg/g)
 Weight of residue in acetone wash: $W_a = C_a V_{aw}$ Pa = $60000(19)(.7858)(.200) = (.0003)$

Run # 1	Run # 2	Run # 3
200	200	200
157.2445	132.7749	163.0370
157.2411	132.7735	163.0351
157.2418	132.7742	163.0360
157.2005	132.7545	162.9957
0003	0003	0003
.0410	.0194	.0410

Acetone rinse volume (Vaw) 200 ml
 Date/Time of wt 2/3/88 3.15 pm gross wt g
 Date/Time of wt 2/4/88 8.30 am gross wt g
 Average Gross wt g
 Tare wt g
 Less acetone blank wt (Wa) g
 Wt of particulate in acetone rinse (ma) g

Filter Numbers
 Date/Time of wt 2/3/88 3.15 pm gross wt g
 Date/Time of wt 2/4/88 8.30 am gross wt g
 Average Gross wt g
 Tare wt g

Weight of particulate on filters(s) (mf) g	.0692	.0305	.0556
Weight of particulate in acetone rinse g	.0410	.0194	.0410
Total weight of particulate (m _t) g	.1102	.0499	.0966

Note: In no case should a blank residue greater than 0.01 mg/g (or 0.001% of the blank weight) be subtracted from the sample weight.

Remarks

Signature of analyst Jim Roe Signature of reviewer [Signature]

VII. CALCULATIONS

NAME: PIEDMONT ASPHALT

LOCATION: GOLD HILL, NORTH CAROLINA

date

2/01/88

2/02/88

SUMMARY OF TEST DATA

RUN # 1

RUN # 2

SAMPLING TRAIN DATA

start

14:32

08:30

10:11

finish

15:43

09:35

11:11

1 Sampling time, minutes

θ

64

64

64

2 Sampling nozzle diameter, in.

Dn

.230

.230

.230

3 Sampling nozzle cross-sectional area, ft.²

An

.000289

.000289

.000289

4 Isokinetic variation

I

104

103

103

5 Sample gas volume - meter conditions, cf.

Vm

38.08

35.46

34.21

6 Average meter temperature, °R

Tm

554

546

554

7 Average orifice pressure drop, in. H₂O

ΔH

1.07

.97

.86

8 Total particulate collected mg.

Mn

110.2

49.9

96.6

VELOCITY TRAVERSE DATA

9 Stack area, ft.²

A

5.1

5.1

5.1

10 Absolute stack gas pressure, in. Hg.

Ps

29.58

29.58

29.58

11 Barometric pressure, in. Hg.

Pbar

29.58

29.58

29.58

12 Average absolute stack temperature, °R

Ts

743

735

73

13 Average $\sqrt{\text{velocity head}}$, (Cp = .79) $\sqrt{\Delta P}$

.92

.86

.86

14 Average stack gas velocity ft. / sec.

Vs

61

56

51

STACK MOISTURE CONTENT

15 Total water collected by train, ml.

Vic

275.0

235.0

233.0

16 Moisture in stack gas, %

Bws

26.2

24.4

25.1

EMISSIONS DATA:

17 Stack gas flow rate, dscf/hr. (1000's)

Qsd

583

558

531

18 Total particulate concentration, gr/dscf

Cs

.0467

.0224

.0451

19 Total particulate concentration, lbs/hr

E

3.9

1.8

3.1

20 Total particulate concentration, lbs/mbtu

E'

.0000

.0000

.0000

ORSAT DATA

21 Percent CO₂ by volumeCO₂

5.3

6.5

7.1

22 Percent O₂ by volumeO₂

10.8

10.8

10.1

23 Percent CO by volume

CO

.0

.0

.0

24 Percent N₂ by volumeN₂

83.9

82.7

82.1

Buzzycaic

Dry Gas Volume :

$$V_{m(std)} = V_m \left[\frac{T_m}{T_{std}} \right] \left[\frac{P_{bar} + \Delta H}{P_{std}} \right] \left[\frac{13.6}{17.64} \right] \frac{1}{R} \frac{1}{Y} \frac{1}{V_m} \frac{1}{P_{bar} + \Delta H} \frac{1}{T_m}$$

Where:

$V_{m(std)}$ = Dry Gas Volume through meter at standard conditions, cu.ft.
 V_m = Dry Gas Volume measured by meter, cu.ft.
 P_{bar} = Barometric pressure at orifice meter, in. Hg.
 P_{std} = Standard absolute pressure, (29.92 in. Hg.)
 T_m = Absolute temperature at meter °R
 T_{std} = Standard absolute temperature (528°R)
 ΔH = Average pressure drop across orifice meter, in. Hg.²
 Y = Dry gas meter calibration factor
 13.6 = Inches water per inches Hg.

$$\text{Run \# 1 } V_{m(std)} = 17.64 (1.01) (38.08)$$

$$\left[\frac{554}{1.07 + \frac{13.6}{(29.58) + \frac{13.6}{554}}} \right]$$

$$= 36.32 \text{ de}$$

$$\text{Run \# 2 } V_{m(std)} = 17.64 (1.01) (35.46)$$

$$\left[\frac{546}{.97 + \frac{13.6}{(29.58) + \frac{13.6}{546}}} \right]$$

$$= 34.31 \text{ de}$$

$$\text{Run \# 3 } V_{m(std)} = 17.64 (1.01) (34.23)$$

$$\left[\frac{555}{.89 + \frac{13.6}{(29.58) + \frac{13.6}{555}}} \right]$$

$$= 32.57 \text{ de}$$

Total contaminants by weight: GRAIN LOADING.

Particulate concentration C_s gr./dscf.

$$C_s = \begin{bmatrix} 0.0154 \text{ mg} \\ \text{gr} \end{bmatrix} \begin{bmatrix} M \\ \frac{V}{n} \end{bmatrix} \begin{bmatrix} \frac{V}{n} \\ V_{m(std)} \end{bmatrix}$$

where:

C_s = Concentration of particulate matter in stack gas, dry basis, corrected to standard conditions, gr./dscf.

M_n = Total amount of particulate matter collected, mg.

$V_{m(std)}$ = Dry gas volume through meter at standard conditions, cu.ft.

$$\text{Run \# 1: } C_s = \begin{bmatrix} 0.0154 \text{ mg} \\ \text{gr} \end{bmatrix} \begin{bmatrix} 110.2 \\ 36.32 \end{bmatrix} = .0467 \text{ gr./dscf.}$$

$$\text{Run \# 2: } C_s = \begin{bmatrix} 0.0154 \text{ mg} \\ \text{gr} \end{bmatrix} \begin{bmatrix} 49.9 \\ 34.31 \end{bmatrix} = .0224 \text{ gr./dscf.}$$

$$\text{Run \# 3: } C_s = \begin{bmatrix} 0.0154 \text{ mg} \\ \text{gr} \end{bmatrix} \begin{bmatrix} 96.6 \\ 32.57 \end{bmatrix} = .0457 \text{ gr./dscf.}$$

Dry molecular weight:

$$M_D = 0.44(\%CO_2) + 0.32(\%O_2) + 0.28(\%CO + \%N_2).$$

where:

M_D	= Dry molecular weight, lb./lb.-mole.
$\%CO_2$	= Percent carbon dioxide by volume (dry basis).
$\%O_2$	= Percent oxygen by volume (dry basis).
$\%N_2$	= Percent nitrogen by volume (dry basis).
$\%CO$	= Percent carbon monoxide by volume (dry basis).
0.264	= Ratio of O_2 to N_2 in air, v/v.
0.28	= Molecular weight of N_2 or CO , divided by 100.
0.32	= Molecular weight of O_2 divided by 100.
0.44	= Molecular weight of CO_2 divided by 100.

Run # 1:

$$M_D = 0.44(5.3\%) + 0.32(10.8\%) + 0.28(.0\% + 83.9\%) = 29.3$$

lb./lb.-mo

Run # 2:

$$M_D = 0.44(6.5\%) + 0.32(10.8\%) + 0.28(.0\% + 82.7\%) = 29.5$$

lb./lb.-mo

Run # 3:

$$M_D = 0.44(7.8\%) + 0.32(10.0\%) + 0.28(.0\% + 82.2\%) = 29.6$$

lb./lb.-mo

Water vapor condensed :

$$V_{wc}^{std} = \left[V_f - V_i \right] \left[\frac{P_w}{P} \frac{R T^{(std)}}{T^{(std)}} \frac{M_w}{M} \right] = 0.04707 \left[V_f - V_i \right]$$

$$V_{ws}^{std} = \left[W_f - W_i \right] \left[\frac{R}{T^{(std)}} \frac{M_w}{M} \frac{P^{(std)}}{P} \right] = 0.04715 \left[W_f - W_i \right]$$

Where :

0.04707 = Conversion factor ft³/ml.0.04715 = Conversion factor ft³/g.

V_{wc}^{std} = Volume of water vapor condensed (standard conditions) scf.
 V_{ws}^{std} = Volume of water vapor collected in silica gel (standard conditions)
 V_f = Final volume of impinger contents, ml.
 V_i = Initial volume of impinger contents
 P = Density of water, (0.002201 lb/ml).
 R = Ideal gas constant, 21.85 (in.Hg.)(cu.ft./lb.-mole)(°R)
 M_w = Molecular weight of water vapor (18.0 lb/lb-mole).
 T^{std} = Absolute temperature at standard conditions, 528°R.
 P^{std} = Absolute pressure at standard conditions, 29.92 inches Hg.

Run # 1: $V_{wc}^{(std)} = (0.04707) (260.0) = 12.2$ cu.ft
 $V_{ws}^{(std)} = (0.04715) (15.0) = .7$ cu.ft

Run # 2: $V_{wc}^{(std)} = (0.04707) (220.0) = 10.4$ cu.ft
 $V_{ws}^{(std)} = (0.04715) (15.0) = .7$ cu.ft

Run # 3: $V_{wc}^{(std)} = (0.04707) (218.0) = 10.3$ cu.ft
 $V_{ws}^{(std)} = (0.04715) (15.0) = .7$ cu.ft

Moisture content of stack gases:

$$R_{ws} = \frac{V_{wc}^{std} + V_{ws9}^{std} + V_{wc}^{std} + V_{ws9}^{std} + V_{wc}^{std} + V_{ws9}^{std}}{V_{wc}^{std} + V_{ws9}^{std} + V_{wc}^{std} + V_{ws9}^{std} + V_{wc}^{std} + V_{ws9}^{std}} \times 100$$

Where:

 R_{ws} = Proportion of water vapor, by volume, in the gas stream. V_w = Dry gas volume measured by dry gas meter, (dctf). V_{wc}^{std} = Volume of water vapor condensed corrected to standard conditions (scf). V_{ws9}^{std} = Volume of water vapor collected in silica gel corrected to standard conditions (scf).

$$\text{Run \# 1: } R_{ws} = \frac{12.2 + .7}{12.2 + .7 + 36.32} \times 100 = 26.2 \%$$

$$\text{Run \# 2: } R_{ws} = \frac{10.4 + .7}{10.4 + .7 + 34.31} \times 100 = 24.4 \%$$

$$\text{Run \# 3: } R_{ws} = \frac{10.3 + .7}{10.3 + .7 + 32.57} \times 100 = 25.2 \%$$

Molecular weight of stack gases: $M_s = M_d (1 - R_{ws}) + 18 (R_{ws})$.

Where:

 M_s = Molecular weight of stack gas, wet basis, (lb./lb.-mole). M_d = Molecular weight of stack gas, dry basis, (lb./lb.-mole).

$$\text{Run \# 1: } M_s = 29.3 (1 - .262) + 18 (.262) = 26.3 \text{ (lb./lb.-mole).}$$

$$\text{Run \# 2: } M_s = 29.5 (1 - .244) + 18 (.244) = 26.7 \text{ (lb./lb.-mole).}$$

$$\text{Run \# 3: } M_s = 29.6 (1 - .252) + 18 (.252) = 26.7 \text{ (lb./lb.-mole).}$$

Stack gas velocity:

(21)

$$V_s = K_p C_p \left[\frac{\Delta p}{T_s(\text{avg.})} \right]^{1/2} \frac{P_s}{M_s}$$

Where:

- V_s = Average velocity of gas stream in stack, ft./sec.
- K_p = 85.49 ft/sec $\left[\frac{(g/g\text{-mole}) \cdot (mm\ Hg)}{(^{\circ}K)} \right]^{1/2}$
- C_p = Pitot tube coefficient, (dimensionless)
- Δp = Velocity head of stack gas, in. H_2O .
- P_{bar} = Barometric pressure at measurement site, (in. Hg).
- P_g = Stack static pressure (in. Hg).
- P_s = Absolute stack gas pressure, (in. Hg) = $P_{bar} + P_g$
- P_{std} = Standard absolute pressure, (29.92 in. Hg).
- t_s = Stack temperature, ($^{\circ}F$).
- T_s = Absolute stack temperature, ($^{\circ}R$). = $460 + t_s$.
- M_s = Molecular weight of stack gas, wet basis, (lb/lb-mole).

Run # 1:

$$V = (85.49) (.79) (.92)$$

743 283

$$(29.58)(26.34)$$

=

60.68 ft/s

Run # 2:

$$V = (85.49) (.79) (.86)$$

735

$$(29.58)(26.69)$$

=

56.04 ft/s

Run # 3:

$$V = (85.49) (.79) (.83)$$

730

$$(29.58)(26.68)$$

=

53.91 ft/s

Stack gas flow rate:

$$Q_{sd} = 3600 \left[\frac{1 - B_{wc}}{V_s A} \right] \left[\frac{T_{std}}{T_{stk}} \right] \left[\frac{P_s}{P_{std}} \right]$$

Where:

- Q_{sd} = Dry volumetric stack gas flow rate corrected to standard conditions, (dscf/hr).
 A = Cross sectional area of stack (ft.²)
 3600 = Conversion factor, sec./hr.
 t_s = Stack temperature (°f).
 T_s = Absolute stack temperature, (°R).
 T_{std} = Standard absolute temperature, (528°R).
 P_{bar} = Barometric pressure at measurement site, (in.Hg.).
 P_g = Stack static pressure, (in.Hg.).
 P_s = Absolute stack gas pressure, (in.Hg.); $P_s = P_{bar} + P_g$
 P_{std} = Standard absolute pressure, (29.92 in.Hg.).

Run # 3:

$$Q_{sd} = 3600 (1 - .252) (53.91) (5.1)$$

$$= \left[\frac{528}{730} \right] \left[\frac{29.58}{29.92} \right]$$

Run # 2:

$$Q_{sd} = 3600 (1 - .244) (56.04) (5.1)$$

$$= \left[\frac{528}{735} \right] \left[\frac{29.58}{29.92} \right]$$

Run # 1:

$$Q_{sd} = 3600 (1 - .262) (60.68) (5.1)$$

$$= \left[\frac{528}{743} \right] \left[\frac{29.58}{29.92} \right]$$

583302 dsc

557844 dsc

534599 dsc

Emissions rate from stack:

$$E = \frac{(C_s)(Q_{sd})}{7000 \text{ gr./lb.}} = \text{lb. / hr.}$$

Where:

E = Emissions rate, lb./hr.

C = Concentration of particulate matter in stack gas, dry basis, corrected to standard conditions (gr/dscf).
 Q = Dry volumetric stack gas flow rate corrected to standard conditions, (dscf/hr).

$$\text{Run \# 1: } E = \frac{7000}{(.0467)(583302)} = 3.9 \text{ lb. / hr.}$$

$$\text{Run \# 2: } E = \frac{7000}{(.0224)(557844)} = 1.8 \text{ lb. / hr.}$$

$$\text{Run \# 3: } E = \frac{7000}{(.0457)(534599)} = 3.5 \text{ lb. / hr.}$$

Isokinetic variation : $I = 100 T_s$

$$0.002669 V_{ic} + (V_m/T_m)(P_{bar} + \Delta H/13.6) \\ \frac{60}{V_s} \frac{O}{P_s} \frac{A_n}{A_n}$$

Where:

I = Percent isokinetic sampling.

100 = Conversion to percent.

 T_s = Absolute average stack gas temperature, °R.0.002669 = Conversion factor, $Hg - ft^3/ml - ^\circ R$. V_{ic} = Total volume of liquid collected in impingers and silica gel. T_m = Absolute average dry gas meter temperature, °R. P_{bar} = Barometric pressure at sampling site, (in.Hg). ΔH = Average pressure differential across the orifice meter, (in.Hg).

13.6 = Specific gravity of mercury.

60 = Conversion seconds to minutes

O = Total sampling time, minutes.

 V_s = Stack gas velocity, ft./sec. P_s = Absolute stack gas pressure, in.Hg. A_n = Cross sectional area of nozzle, ft^2 .

Run # 1:

I = 100

X 743

$$\frac{60 (64) (53.91) (29.58) (0.00289)}{(0.002669)(275.0) + 554} \\ \frac{38.1}{29.58 + 13.6} = 104$$

Run # 2:

I = 100

X 735

$$\frac{60 (64) (56.04) (29.58) (0.00289)}{(0.002669)(235.0) + 546} \\ \frac{35.5}{29.58 + 13.6} = 103$$

Run # 3:

I = 100

X 730

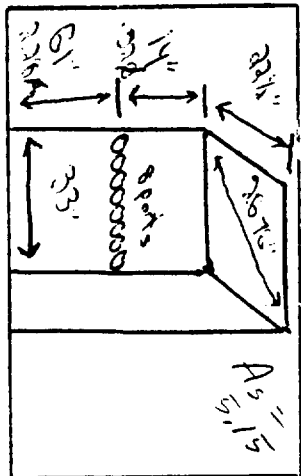
$$\frac{60 (64) (53.91) (29.58) (0.00289)}{(0.002669)(233.0) + 555} \\ \frac{34.2}{29.58 + 13.6} = 102$$

VIII. FIELD DATA

RAMCON ENVIRONMENTAL CORPORATION

Plant Piedmont Asphalt
Weathering

Location Cold Hill Water Conditioning
 Operator Samuel Greenwald
 Date 2/1/88
 Run No. 1
 Sample Box No. 2
 Meter Box No. 1178107 CNA
 Meter H @ 1.74
 C Factor 1.01
 Pitot Tube Coefficient Cp 0.79



Schematic of Stack Cross Section

Ambient Temperature 78°
 Barometric Pressure 29.98
 Assumed Moisture, % 85
 Probe Length, m(ft) 2.54
 Nozzle Identification No. 00000000
 Avg. Calibrated Nozzle Dia., (in.) 0.000000
 Probe Heater Setting 5
 Leak Rate, m³/min. (cfm) 0.000000
 Probe Liner Material 316 Stainless Steel
 Static Pressure, mm Hg (in. Hg) 0.05
 Filter No. 25-2576

TRAV. PT NO.	SAMPLING TIME (θ) min.	VACUUM in. Hg	STACK TEMP (Ts) °F	VELOCITY HEAD (Ps) in H2O	PRESSURE DIFF. ORF. MTR in H2O	GAS SAMPLE VOLUME ft ³	GAS SAMPLE TEMP. AT DRY GAS METER °F		FILTER HOLDER TEMP °F	GAS TEMP AVG CONDENSER OR LAST IMPINGER °F
							Inlet	Outlet		
1	11:33:11	3	237	0.68	0.85	1.00	80	75	210	55
2	11:33:30	4	261	0.81	1.05	1.00	80	75	250	55
3	11:33:48	5	261	0.81	1.15	1.00	80	75	250	55
4	11:34:00	5	264	0.80	1.10	1.00	85	75	250	55
5	11:34:13	5	277	0.85	0.81	1.00	85	75	250	55
6	11:34:35	5	264	0.70	0.81	1.00	85	75	250	55
7	11:34:55	5	264	0.83	1.05	1.00	80	75	250	55
8	11:35:17	5	263	0.81	1.15	1.00	80	75	250	55
9	11:35:39	5	263	0.81	1.15	1.00	80	75	250	55
10	11:35:51	5	263	0.83	0.78	1.00	85	75	250	55
11	11:36:11	5	263	0.83	0.78	1.00	85	75	250	55
12	11:36:30	5	263	0.77	0.85	1.00	85	75	250	55
13	11:36:50	5	265	0.80	1.50	1.00	85	75	250	55
14	11:37:10	5	265	0.81	0.85	1.00	85	75	250	55

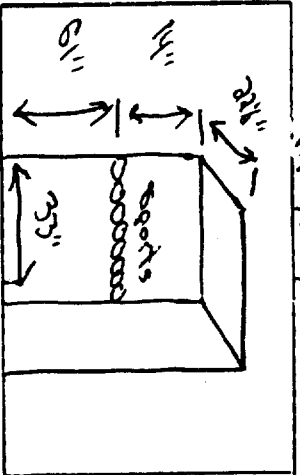
RAMCON emissions test log sheet, cont. DATE 2/1/80 LOCATION Edwards TEST NO. 1

TRAVERSE POINT	SAMPLING TIME (min)	VACUUM (in. Hg)	STACK TEMP (°F)	VELOCITY HEAD (in. H ₂ O)	ORIFICE DIFF. PRESSURE (in. H ₂ O)	GAS VOLUME Vm (l./3)	GAS SAMPLE TEMP. (°F)		SAMPLE BOX TEMP. (°F)	IMPINGER TEMP (°F)
							in	out		
2	15.03	3	285	0.99	0.73	136.69	105	80	280	60
3	15.05	4	286	0.75	0.93	131.86	110	85	280	60
4	15.07	5	284	1.30	1.60	129.22	110	85	285	60
5	15.09	3	283	0.57	0.71	140.33	110	85	285	60
6	15.10	3	286	0.60	0.71	141.31	110	85	285	60
7	15.11	4	288	0.73	0.91	141.74	110	85	285	60
8	15.12	5	280	1.50	1.60	135.88	115	85	280	60
9	15.14	3	285	0.71	0.58	141.83	110	85	285	60
10	15.15	3	286	0.55	0.64	145.76	110	85	285	60
11	15.16	3	286	0.55	1.10	147.03	110	85	285	60
12	15.17	3	280	1.30	1.60	146.17	115	85	285	60
13	15.18	3	280	0.57	0.67	149.11	110	85	285	60
14	15.19	3	287	0.61	0.79	150.54	110	85	280	60
15	15.20	3	286	0.64	1.20	151.60	110	85	280	60
16	15.21	3	286	0.64	1.30	153.10	110	85	280	60
17	15.22	3	286	0.60	1.20	151.74	110	85	280	60
18	15.23	3	286	1.10	1.30	150.07	110	85	280	60
19	15.24	3	286	1.30	1.60	155.07	110	85	280	60
20	15.25	3	286	1.30	1.60	155.74	110	85	280	60
21	15.26	3	286	1.30	1.60	155.07	110	85	280	60
22	15.27	3	286	1.30	1.60	155.07	110	85	280	60
23	15.28	3	286	1.30	1.60	155.07	110	85	280	60
24	15.29	3	286	1.30	1.60	155.07	110	85	280	60
25	15.30	3	286	1.30	1.60	155.07	110	85	280	60
26	15.31	3	286	1.30	1.60	155.07	110	85	280	60
27	15.32	3	286	1.30	1.60	155.07	110	85	280	60
28	15.33	3	286	1.30	1.60	155.07	110	85	280	60
29	15.34	3	286	1.30	1.60	155.07	110	85	280	60
30	15.35	3	286	1.30	1.60	155.07	110	85	280	60

RAMCON ENVIRONMENTAL CORPORATION

8.82

Plant Shaw's Dairy
 Location Shaw's Dairy, North Carolina
 Operator K. H. Hurdinger
 Date 2-2-88
 Run No. 2
 Sample Box No. 11980/2174
 Meter Box No. 1174
 Meter H @ 101
 C Factor 101
 Pitot Tube Coefficient Cp 0.79



Schematic of Stack Cross Section

Ambient Temperature 55
 Barometric Pressure 29.98
 Assumed Moisture, % 8
 Probe Length, m(ft) 381
 Nozzle Identification No. 220
 Avg. Calibrated Nozzle Dia., (in.) 2.20/2.30/2.35
 Probe Heater Setting 5
 Leak Rate, m³/min. (cfm) 4.015 @ 7"
 Probe Liner Material 316 Stainless Steel
 Static Pressure, mm Hg (in. Hg) 0.05
 Filter No. DA-2285

TRAV. PT NO.	SAMPLING TIME (h)min.	VACUUM in. Hg	STACK TEMP (T _s) °F	VELOCITY HEAD (P _s) in H ₂ O	PRESSURE DIFF. ORF. MTR in H ₂ O	GAS SAMPLE VOLUME ft ³	GAS SAMPLE TEMP. AT DRY GAS METER °F		FILTER HOLDER TEMP °F	GAS TEMP LVS CONDENSER OR LAST IMPINGER °F
							Inlet	Outlet		
1	8:30:45 8:32	2	245	.55	.48	13.43 140.33	70	65	240	60
2	8:34	3	250	.70	.87	141.38	80	65	240	60
3	8:36	3	255	.75	.93	142.48	80	65	245	55
4	8:38:45	4	260	.78	.97	143.605	85	65	245	55
5	8:39:30 8:41	2	260	.55	.68	144.78	85	65	245	55
6	8:43	2	265	.55	.68	145.52	90	70	245	55
7	8:45	4	265	.75	.93	146.64	90	70	250	55
8	8:47:30	4	270	.80	.95	147.765	95	70	250	55
9	8:49:45 8:49	2	270	.40	.50	148.62	95	70	250	55
10	8:51	3	270	.55	.68	149.58	95	70	250	55
11	8:53	4	275	.75	.93	170.72	100	70	250	55
12	8:55:45	4	275	.75	.93	171.80	100	70	250	55
13	8:56 8:58	2	275	.45	.56	172.72	100	75	255	55

RAMCON

emissions test log sheet, cont.

DATE 2-2-85

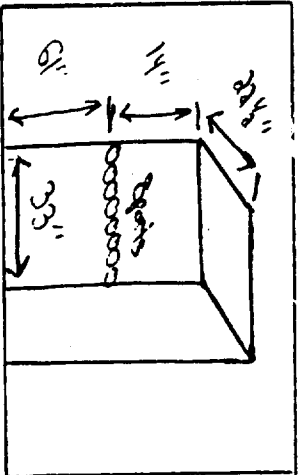
LOCATION 2000 HILLTEST NO. 2

TRAVERSE POINT	SAMPLING TIME (min)	VACUUM mm Hg (in. Hg)	STACK TEMP T _s (°F)	VELOCITY HEAD AP _s (in. H ₂ O)	ORIFICE DIFF. PRESSURE ΔH (in. H ₂ O)	GAS VOLUME V _m (ft. ³)	GAS SAMPLE TEMP. (°F)		SAMPLE BOX TEMP. (°F)	IMPINGER TEMP (°F)
							in	out		
2	9:00	2	275	.45	.56	173.60	100	75	255	55
3	9:02	3	275	.55	.68	174.69	100	75	255	55
4	9:04	5	280	.55	1.2	175.835	100	75	255	55
2	9:04:30 9:06	2	280	.40	.50	174.73	100	75	255	55
2	9:08	2	280	.45	.56	177.41	100	75	260	55
3	9:10	3	280	.58	.68	178.58	100	75	260	55
4	9:12:30	5	285	.95	1.2	174.845	105	75	260	55
2	9:13 9:15	2	280	.45	.56	180.72	100	80	260	55
2	9:17	2	285	.45	.56	181.60	105	80	260	55
3	9:19	4	285	1.0	1.2	182.83	105	80	260	55
4	9:21	5	285	1.1	1.4	184.65	105	80	260	55
2	9:21:03 9:23	2	285	.50	.62	185.16	105	80	260	55
2	9:25	3	285	.55	.68	186.12	105	80	260	55
3	9:27	5	285	1.3	1.6	187.52	105	80	260	55
4	9:29:15	6	290	1.6	2.0	185.07	110	80	260	55
4	9:25:40	5	280	1.0	1.2	190.50	105	80	255	55
2	9:31	5	285	1.2	1.5	191.74	105	80	255	55
3	9:33	6	285	1.5	1.9	193.26	110	80	255	55
4	9:35:40	6	285	1.6	2.0	194.852	110	80	255	55

RAMCON ENVIRONMENTAL CORPORATION

8.052

Plant Shell Refining
 Location South Carolina
 Operator K. Williams
 Date 2-2-88
 Run No. 3
 Sample Box No. 117801
 Meter Box No. 117801
 Meter H @ 101
 C Factor 1.01
 Pitot Tube Coefficient Cp 0.98



Schematic of Stack Cross Section

Ambient Temperature 65
 Barometric Pressure 29.98
 Assumed Moisture, % 3.5
 Probe Length, m(ft) 35
 Nozzle Identification No. 0002885
 Avg. Calibrated Nozzle Dia., (in.) 1.230/1.234
 Probe Heater Setting 5
 Leak Rate, m³/min. (cfm) 4.0/6.07
 Probe Liner Material 316 Stainless Steel
 Static Pressure, mm Hg (in. Hg) 0.05
 Filter No. 25 2178

TRAV. PT NO.	SAMPLING TIME (h) min.	VACUUM in. Hg	STACK TEMP (Ts) °F	VELOCITY HEAD (Ps) in H2O	PRESSURE DIFF. ORF. MTR in H2O	GAS SAMPLE VOLUME ft ³	GAS SAMPLE TEMP. AT DRY GAS METER °F		FILTER HOLDER TEMP °F	GAS TEMP LVC CONDENSER OR LAST IMPINGER °F
	10:12:10 10:12:18	2	260	.75	.93	185.336 184.44	90	85	235	60
2	10:30	4	270	1.3	1.4	157.51	95	80	240	60
3	10:32	4	270	1.3	1.4	158.71	100	80	240	60
4	10:34:20	5	270	1.4	1.7	199.92	95	80	240	60
1	10:33 10:37	3	245	.55	.68	200.90	95	80	240	55
2	10:39	3	270	.63	.78	202.04	100	80	240	55
3	10:41	5	270	1.0	1.2	203.33	100	80	245	55
4	10:43	5	275	1.1	1.4	204.81	100	80	245	55
1	10:43:10 10:45	2	270	.40	.50	205.66	100	80	245	55
2	10:47	2	270	.40	.50	206.58	100	80	250	55
3	10:49	3	270	.78	.97	207.72	105	80	250	55
4	10:51:40	5	235 236	1.2	1.5	208.134	110	80	250	55
1	10:52:10 10:54	2	210 210	.40	.50	209.02	100	80	250	55

RAMCON

emissions test log sheet, cont.

DATE 2-2-88

LOCATION 6000 W. NC

TEST NO. 3

TRAVERSE POINT	SAMPLING TIME (min)	VACUUM (in. Hg)	STACK TEMP. T _s (°F)	VELOCITY HEAD AP _s (in. H ₂ O)	ORIFICE DIFF. PRESSURE ΔH (in. H ₂ O)	GAS VOLUME V _m (ft. ³)	GAS SAMPLE TEMP. (°F)		SAMPLE BOX TEMP. (°F)	IMPIINGER TEMP (°F)
							in	out		
2	10:54	2	270	.45	.55	210.90	105	85	255	55
3	10:58	2	270	.45	.55	211.78	110	85	255	55
4	11:00:45	4	275	.55	1.2	213.052	110	85	260	55
2	11:01:15	2	265	.40	.50	213.53	110	85	260	55
2	11:05	2	270	.45	.55	214.83	110	85	260	55
3	11:07	2	270	.50	.62	215.77	110	85	260	55
4	11:09:15	4	270	.87	1.1	216.971	110	85	260	55
2	11:09:30	2	265	.43	.53	217.79	110	85	260	55
2	11:13	2	270	.43	.53	218.67	110	85	260	55
3	11:15	3	270	.60	.74	219.63	110	85	255	55
4	11:17:50	5	270	.80	.99	220.80	110	85	255	55
2	11:18:30	3	265	.45	.56	221.71	110	85	255	55
2	11:22	2	270	.52	.64	222.67	110	85	255	55
3	11:24	3	270	.70	.87	223.77	110	85	255	55
4	11:26:20	3	270	.83	1.0	224.937	115	85	255	55
4	11:28:15	2	265	.50	.62	225.89	110	85	255	55
2	11:30	3	270	.77	.95	227.04	115	85	255	55
3	11:32	3	275	.90	1.1	228.29	115	90	255	55
2	11:34:45	3	275	.90	1.1	229.562	115	90	255	55

IX. CALIBRATIONS

METER BOX CALIBRATION DATA AND CALCULATION FORM

(English units)

Date 2-3-58 Meter box number 147810 (C-124)Barometric pressure, $P_b = 29.55$ in. Hg Calibrated by MA

Orifice manometer setting (ΔH), in. H_2O		Gas volume		Temperature				Time (θ), min	Y_i	$\Delta H_{H_2O}^I$
Wet test meter (V^w), ft ³	Dry gas meter (V^d), ft ³	Wet test meter (t^w), of	Wet test meter (t^w), of	Inlet (t_d^i), of	Outlet (t_d^o), of	Avg (t_d), of				
0.5	5	26.946 27.235	68	100 75	87.5 75	12.23	1.0000	1.66		
1.0	5	26.253 26.743	68	100 75	88 75	8.52	1.0046	1.70		
1.5	10	25.147 26.171	68	100 70	86.75 70	14.12	1.0114	1.69		
2.0	10									
3.0	10									
4.0	10									
		Avg				1.68				

$\Delta H, \text{ in. } H_2O$	$\frac{13.6}{\Delta H}$	$Y_i = \frac{V^w P_b (t_d + 460)}{V^d (P_b + \frac{13.6}{\Delta H}) (t + 460)}$	$\Delta H_{H_2O}^I = \frac{P_b (t_d + 460)}{0.0317 \Delta H} \left[\frac{V^w}{(t_w + 460) \theta} \right]$
0.5	0.0368	$\frac{5.2485 \cdot 547.5}{5.078 (29.55 + 0.528) 528}$	$\frac{1.0000}{1.66}$
1.0	0.0737	$\frac{5.2485 \cdot 547.5}{5.153 (29.55 + 0.735) 528}$	$\frac{1.0046}{1.70}$
1.5	0.110	$\frac{10.2589 \cdot 546.75}{10.201 (29.55 + 1.103) 528}$	$\frac{1.0114}{1.69}$
2.0	0.147		
3.0	0.221		
4.0	0.294		

^a If there is only one thermometer on the dry gas meter, record the temperature under t_d .

METER BOX CALIBRATION DATA AND CALCULATION FORM

(English units)

Date

11-6-87

Meter box number

147510

Barometric pressure, $P_b = 29.84$ in. Hg Calibrated by *MS*

Office manometer setting (ΔH), in. H_2O	Gas volume		Temperature				Time min	Y_i	$\Delta H_{H_2O}^i$
	Wet test meter	Dry gas meter	Wet test meter	Inlet (t_D^i), of	Outlet (t_D^o), of	Avg (t_D), of			
0.5	5	64.57	71.6	102	104	92	12.24	1.0069	1.67
1.0	5	55.55	71.6	104	107	92	5.59	1.0125	1.75
1.5	10	48.36	71.6	102	95	97.5	14.47	1.0161	1.78
2.0	10								
3.0	10								
4.0	10								
Avg									1.74

$\Delta H_{H_2O}^i$, in. H_2O	$\frac{\Delta H}{13.6}$	$Y_i = \frac{V_P(t_D + 460)}{V_P(t_D + 460) + \frac{\Delta H}{13.6} P_b} = \frac{V_P(t_D + 460)}{V_P(t_D + 460) + 0.0317 \Delta H P_b}$	$\Delta H_{H_2O}^i = \frac{0.0317 \Delta H P_b}{(t_D + 460) \theta} \left[\frac{V_P}{V_P + 460} \right]$
0.5	0.0368		
1.0	0.0737		
1.5	0.110		
2.0	0.147		
3.0	0.221		
4.0	0.294		

^a If there is only one thermometer on the dry gas meter, record the temperature under t_D .

Lear Siegler Stack Sampler

Nozzle Diameter Calibration

Date

Signature

Nozzle No. Average Diameter

Nozzle No. Average Diameter

1
2
3
4
5
6

7
8
9
10
11
12

Pitot Tube Calibration (S Type)

Pitot Tube Identification No. 33

Calibrated by: C. M. K. 100

Date

9-5-87

"A" SIDE CALIBRATION

Impact

Run No.	Δp std cm H ₂ O (In. H ₂ O)	Δp (s) cm H ₂ O (In. H ₂ O)	C_p (s)	DEVIATION $C_p(s) - \bar{C}_p(A)$
1	1.10	1.70	0.804	+0.009
2	0.56	0.88	0.798	+0.003
3	0.33	0.54	0.782	-0.01
		$\bar{C}_p$ (SIDE A)	0.795	

"B" SIDE CALIBRATION

Run No.	Δp std cm H ₂ O (In. H ₂ O)	Δp (s) cm H ₂ O (In. H ₂ O)	C_p (s)	DEVIATION $C_p(s) - \bar{C}_p(B)$
1	1.10	1.70	0.804	+0.003
2	0.56	0.87	0.802	+0.001
3	0.33	0.52	0.797	-0.004
		$\bar{C}_p$ (SIDE B)	0.801	

AVERAGE DEVIATION = σ (A OR B) = $\frac{1}{3} |C_p(s) - \bar{C}_p(A \text{ OR } B)|$

→ MUST BE < 0.01

$|C_p(\text{SIDE A}) - \bar{C}_p(\text{SIDE B})| \rightarrow \text{MUST BE} < 0.01$

$$C_p(s) = C_p(\text{std}) \sqrt{\frac{\Delta p}{\Delta p_s}}$$

RAMCON ENVIRONMENTAL CORPORATION

Date 9-5-87
Thermocouple number Indef
Ambient temperature 83 °F Barometric pressure 30.52 in. Hg
Calibrator C. McLeod Reference: mercury-in-glass
other _____

Reference point numbers	Source ^b (specify)	Reference Thermometer Temperature, °F	Thermocouple Potentiometer Temperature, °F	Temperature Difference, °C
A	Ice bath	33	33	0
B	oven	150	150	0
C	oven	175	175	0
D	Ambient	83	83	0
	2-1-88	72	72	0

a Every 30°C (50°F) for each reference point.

b Type of calibration system used.

$$\left[\frac{(\text{ref temp, } ^\circ\text{C} + 273) - (\text{test thermom temp, } ^\circ\text{C} + 273)}{\text{ref temp, } ^\circ\text{C} + 273} \right] \times 100 < 1.58$$

Figure 2.5 stack temperature sensor calibration data form.

RAMCON ENVIRONMENTAL CORPORATION

Date 9-5-87
Thermocouple number Hotbox #2
Ambient temperature 84 °F Barometric pressure 30.52 in. Hg
Calibrator C.M. Hood Reference: mercury-in-glass
other _____

Reference point number ^a	Source ^b (specify)	Reference Thermometer Temperature, °C	Thermocouple Potentiometer Temperature, °C	Temperature Difference, °C
A	Ice bath	33	33	0
B	Oven	150	150	0
C	Oven	175	175	0
D	Ambient	84	84	0
	2-1-88	72	72	0

^aEvery 30°C (50°F) for each reference point.

^bType of calibration system used.

$$C[(\text{ref temp, } ^\circ\text{C} + 273) - (\text{test thermom temp, } ^\circ\text{C} + 273)]$$
$$\frac{\text{ref temp, } ^\circ\text{C} + 273}{100} < 1.58.$$

Figure 2.5 stack temperature sensor calibration data form.

Lear Siegler Stack Sampler

RAMCON

(50)

Heating Probe Calibration

Probe No. 33

Date of Calibration 1/09/87

Signature

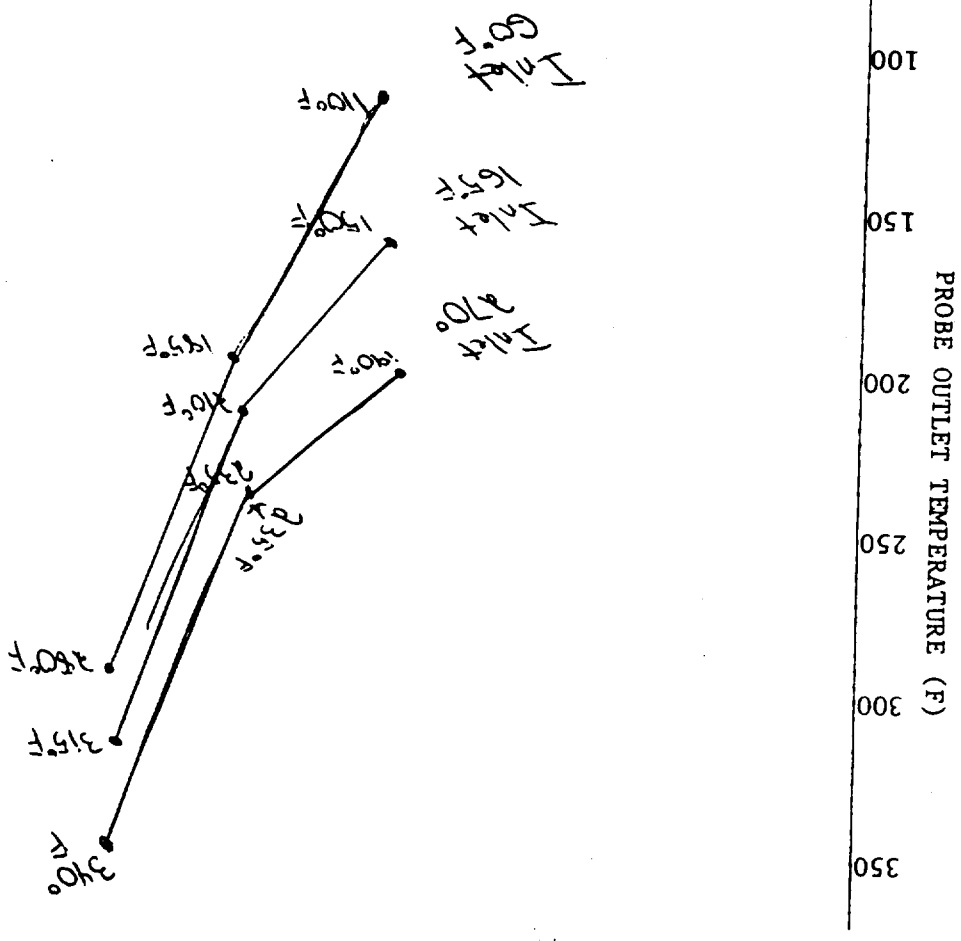
Shawn Sheppard

Probe Length

3 ft.

Name of Company to be tested

Note: 3 ft. probe - 5 min. warmup
6 ft. probe - 15 min. warmup
10 ft. probe - 30 min. warmup
Calibration flow rate = .75 CFM



RAMCON ENVIRONMENTAL CORPORATION

Date 9-5-87
Thermocouple number 33
Ambient temperature 85 °F Barometric pressure 30.52 in. Hg
Calibrator C.M.H.L.O. Reference: mercury-in-glass
other

Reference point numbers	Source ^b (specify)	Reference Thermometer Temperature, °C ^a	Thermocouple Potentiometer Temperature, °C ^a	Temperature Difference, °C ^a
A	Ice bath	33	33	0
B	oven	150	150	0
C	oven	175	175	0
D	Ambient	85	85	0
	Z-1-88	72	72	0

^aEvery 30°C (50°F) for each reference point.

^bType of calibration system used.

$$^{\circ}\text{C} \left[(\text{ref temp, } ^{\circ}\text{C} + 273) - (\text{test thermom temp, } ^{\circ}\text{C} + 273) \right] \left[\frac{\text{ref temp, } ^{\circ}\text{C} + 273}{100} \right] < 1.58.$$

Figure 2.5 stack temperature sensor calibration data form.

X. RAMCON PERSONNEL

X. RAMCON PERSONNEL

RAMCON Environmental Stack Test Team

(38)

Sumner Buck - President

Sumner Buck is the President of RAMCON Environmental. He is a graduate of the EPA 450 "Source Sampling for Particulate Pollutants" course and the 474 "Continuous Emissions Monitoring" course all given at RTP. Mr. Buck is a qualified V.E. reader with current certification. Mr. Buck has personally sampled over 300 stacks including over 200 asphalt plants. He is 43 years old and a graduate of the University of Mississippi with Graduate studies at Memphis State University and State Technical Institute of Memphis.

Ken Allmendinger - Team Leader

Ken Allmendinger has been employed with RAMCON for three years. He has sampled over 100 asphalt plants with extensive training in Methods 1 through 5. He is qualified as a team leader and has current certification as a V.E. reader.

XI. VISIBLE EMISSIONS

(40)

(41)

TENNESSEE AIR POLLUTION CONTROL SMOKE SCHOOL TRAINING FORM
(42)

RUN# 01A SUNGLASSES

COURSE LOCATION St. Louis, Mo.

COMPANY Shawm Overwood

DATE 12/17/77 SKY Cloudy WIND 10 DISTANCE & DIRECTION TO STACK

ERROR

READING #	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25
0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5
1	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100					
2	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100					
3	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100					
4	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100					
5	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100					
6	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100					
7	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100					
8	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100					
9	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100					
10	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100					
11	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100					
12	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100					
13	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100					
14	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100					
15	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100					
16	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100					
17	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100					
18	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100					
19	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100					
20	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100					
21	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100					
22	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100					
23	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100					
24	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100					
25	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100					
DEVIATION																									
1	100	95	90	85	80	75	70	65	60	55	50	45	40	35	30	25	20	15	10	5	0				

26	26	26	26	26	26	26	26	26	26	26	26	26	26	26	26	26	26	26	26	26	26	26	26	26
27	27	27	27	27	27	27	27	27	27	27	27	27	27	27	27	27	27	27	27	27	27	27	27	27
28	28	28	28	28	28	28	28	28	28	28	28	28	28	28	28	28	28	28	28	28	28	28	28	28
29	29	29	29	29	29	29	29	29	29	29	29	29	29	29	29	29	29	29	29	29	29	29	29	29
30	30	30	30	30	30	30	30	30	30	30	30	30	30	30	30	30	30	30	30	30	30	30	30	30
31	31	31	31	31	31	31	31	31	31	31	31	31	31	31	31	31	31	31	31	31	31	31	31	31
32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32
33	33	33	33	33	33	33	33	33	33	33	33	33	33	33	33	33	33	33	33	33	33	33	33	33
34	34	34	34	34	34	34	34	34	34	34	34	34	34	34	34	34	34	34	34	34	34	34	34	34
35	35	35	35	35	35	35	35	35	35	35	35	35	35	35	35	35	35	35	35	35	35	35	35	35
36	36	36	36	36	36	36	36	36	36	36	36	36	36	36	36	36	36	36	36	36	36	36	36	36
37	37	37	37	37	37	37	37	37	37	37	37	37	37	37	37	37	37	37	37	37	37	37	37	37
38	38	38	38	38	38	38	38	38	38	38	38	38	38	38	38	38	38	38	38	38	38	38	38	38
39	39	39	39	39	39	39	39	39	39	39	39	39	39	39	39	39	39	39	39	39	39	39	39	39
40	40	40	40	40	40	40	40	40	40	40	40	40	40	40	40	40	40	40	40	40	40	40	40	40
41	41	41	41	41	41	41	41	41	41	41	41	41	41	41	41	41	41	41	41	41	41	41	41	41
42	42	42	42	42	42	42	42	42	42	42	42	42	42	42	42	42	42	42	42	42	42	42	42	42
43	43	43	43	43	43	43	43	43	43	43	43	43	43	43	43	43	43	43	43	43	43	43	43	43
44	44	44	44	44	44	44	44	44	44	44	44	44	44	44	44	44	44	44	44	44	44	44	44	44
45	45	45	45	45	45	45	45	45	45	45	45	45	45	45	45	45	45	45	45	45	45	45	45	45
46	46	46	46	46	46	46	46	46	46	46	46	46	46	46	46	46	46	46	46	46	46	46	46	46
47	47	47	47	47	47	47	47	47	47	47	47	47	47	47	47	47	47	47	47	47	47	47	47	47
48	48	48	48	48	48	48	48	48	48	48	48	48	48	48	48	48	48	48	48	48	48	48	48	48
49	49	49	49	49	49	49	49	49	49	49	49	49	49	49	49	49	49	49	49	49	49	49	49	49
50	50	50	50	50	50	50	50	50	50	50	50	50	50	50	50	50	50	50	50	50	50	50	50	50
DEVIATION																								

I hereby certify that the above readings are my own.

TENNESSEE AIR POLLUTION CONTROL SMOKE SCHOOL TRAINING FORM (45)

NAME Ken Allmendinger COMPANY Kerrigan
 COURSE LOCATION 5711 RUN# 01 SUNGLASSES _____
 DATE 12-1-87 SKY cl/c WIND 110 DISTANCE & DIRECTION TO STACK 1100 ft
 ERROR _____

1	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
2	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
3	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
4	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
5	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
6	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
7	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
8	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
9	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
10	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
11	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
12	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
13	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
14	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
15	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
16	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
17	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
18	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
19	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
20	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
21	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
22	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
23	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
24	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
25	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100

26	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
27	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
28	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
29	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
30	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
31	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
32	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
33	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
34	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
35	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
36	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
37	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
38	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
39	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
40	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
41	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
42	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
43	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
44	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
45	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
46	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
47	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
48	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
49	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100
50	0.5	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	90	95	100