

AP42 Section: 11.1

Reference Number: 193

Title: Report Of Air Pollution Source Testing For
Particulate Matter At Calmat (Industrial Asphalt
Corp.) Pala Indian Reservation, Pala, CA,

Engineering Science, Irwindale, CA,

February 25, 1990.

**REPORT OF AIR POLLUTION
SOURCE TESTING
FOR PARTICULATE MATTER**

Conducted on:

December 12, 1990

Conducted at:

**CALMAT (INDUSTRIAL ASPHALT CORPORATION)
PALA INDIAN RESERVATION, PALA, CALIFORNIA**

Submitted on:

February 25, 1991

Prepared by:

**Engineering-Science
6060 N. Irwindale Avenue Suite J
Irwindale, CA 90607
Telephone: (818) 969-5758**

**REPORT OF AIR POLLUTION SOURCE TESTING
FOR PARTICULATE MATTER
AT CALMAT (INDUSTRIAL ASPHALT CORPORATION)
PALA INDIAN RESERVATION, PALA, CA**

INTRODUCTION

On December 12, 1990 Engineering-Science, (ES) Pasadena, CA, conducted air pollution source testing on an asphalt batch plant operated by Industrial Asphalt Corporation at their facility at Pala, California. The source tested was the rotary dryer baghouse exhaust stack. The unit is operated under Authority to Construct, Application No. 890709, granted by the San Diego Air Pollution Control District (SDAPCD). Testing was conducted to determine the emission rate of particulate matter.

The testing was coordinated by Mr. Dwight Beavers and Paul Mason of Industrial Asphalt. The testing was observed by Ms. C.W. Ridenour and Mr. G.D. Smith of SDAPCD. Also, Mr. Andy Segal and Mr. Dean Carlson of the SDAPCD did the engineering observation report and production rate sample calculations which are located in Appendix D. The ES testing team was comprised of Messrs. Dennis Bautista (team leader), Dwight J. Wieman, and Nick Nielsen

PROCESS DESCRIPTION

Industrial Asphalt Corporation, a division of Calmat operates a Hot Asphalt Batch Plant at the Pala Indian Reservation in Pala, California.

Aggregate supplied by the Calmat quarry located adjacent to the plant is carried via belt conveyor to the batch plant. To remove moisture, it is heated and dried in a diesel oil fired rotary dryer. This hot aggregate is then mixed with hot asphalt oil to form a "batch". This "batch" is either poured into waiting trucks or stored in silos. The plant can produce a maximum of 225 tons per hour, but normal operating rates are about 200 tons per hour. During the particulate testing the average production rate was 217.8 tons per hour. Figure 1 is a representation of the facilities process diagram.

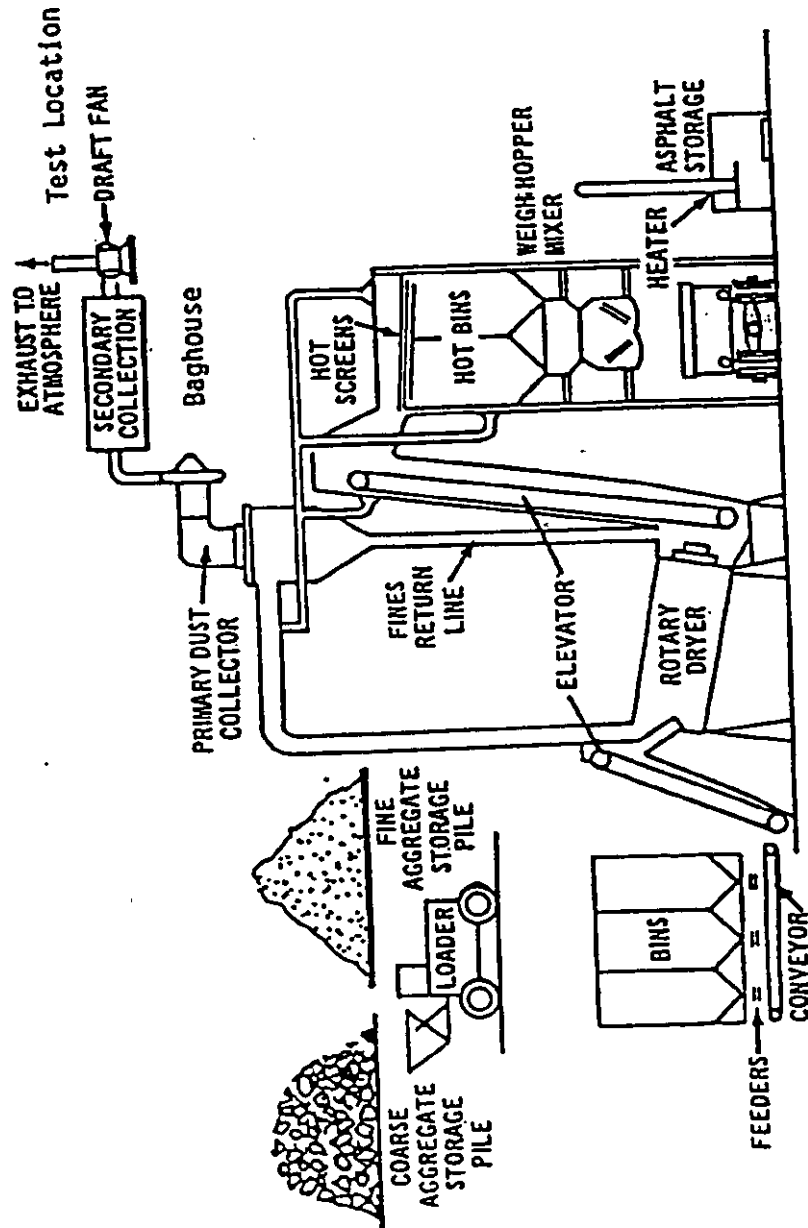
TEST METHODOLOGY

Location and Number of Traverse Points

EPA Method 1 was used to determine the number and location of the traverse points. A 24 point traverse sampling was selected, utilizing two ports.

A cyclonic flow check was conducted at each traverse point. An S-type pitot tube connected to an inclined oil manometer was used for the determination. The pitot

PROCESS DIAGRAM



tube was positioned so the planes of the face openings were perpendicular to the stack cross-sectional plane. This was referred to as the "0°" reference position, the manometer should read zero to indicate no cyclonic flow. If the manometer did not read zero the pitot tube is rotated until a zero reading is obtained. The angle of rotation was measured to the nearest degree. The average of all the rotation angles were 15°. Although cyclonic flow was more than the 10° limit, the test was allowed by SDAPCD.

Stack Velocity and Temperature Traverse

EPA Method 2 was used to determine the velocity of the stack gas and stack gas temperature at the time of the testing. An S-type pitot tube connected to an inclined oil manometer and a K-type (chromel-alumel) thermocouple connected to a temperature read out device were used to traverse the 24 sampling points. The nozzle size required to achieve isokinetic sampling rates were calculated from the measurements.

Stack Gas Molecular Weight

The carbon dioxide (CO₂), oxygen (O₂), and carbon monoxide (CO) concentrations in the stack gas were determined from integrated bag samples collected in Tedlar bags and analyzed by Orsat in accordance with EPA Method 3.

Stack Gas Moisture Content

The moisture content of the stack gas was determined in conjunction with the particulate matter train. The moisture was determined gravimetrically by the weight gain in each impinger in accordance with EPA Method 4.

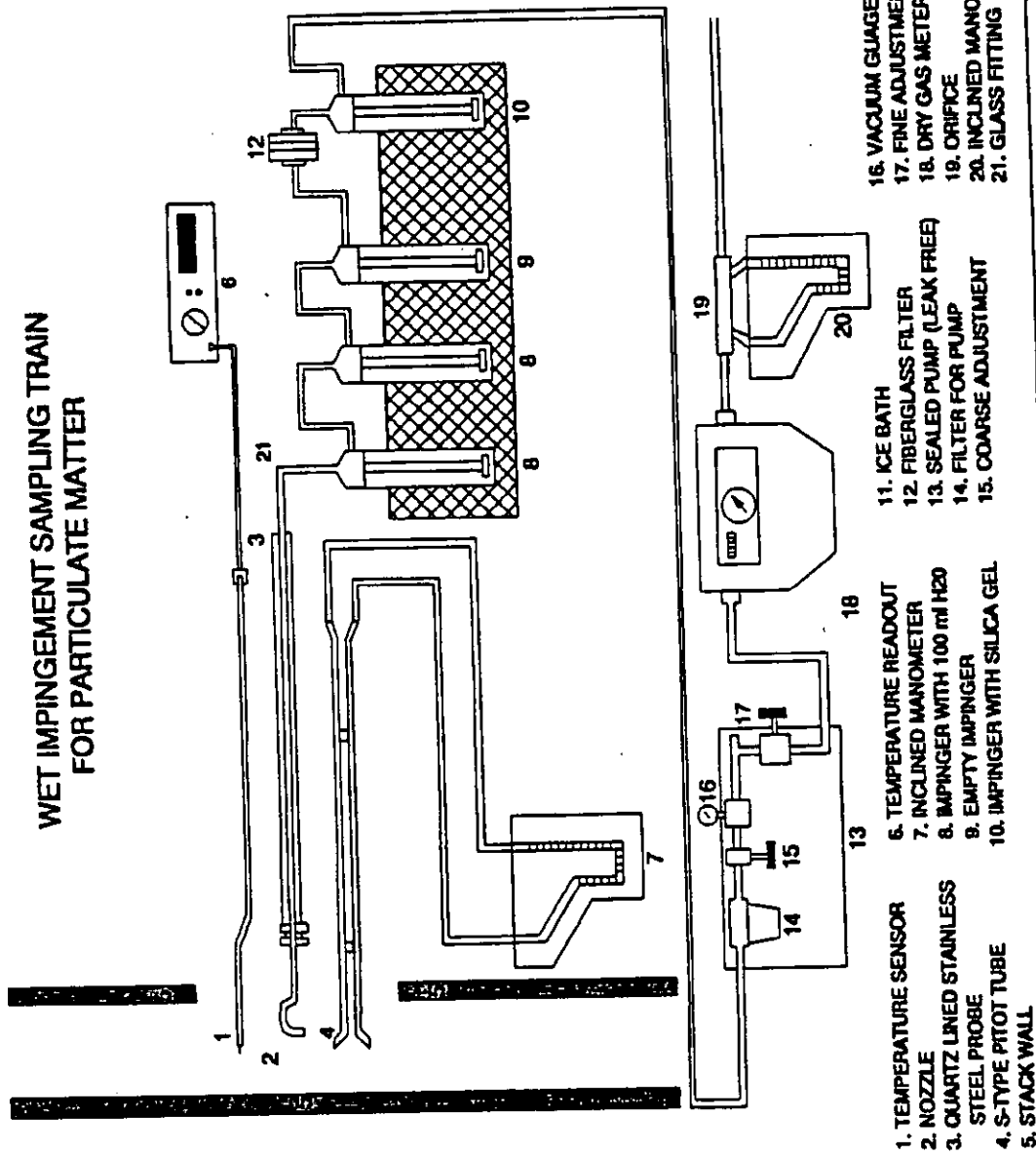
Particulate Matter

The particulate matter sampling train was based on EPA Method 5, modified to exclude the front end filter and include a back end filter to comply with the SDAPCD testing guidelines.

The sampling train was comprised of a quartz lined heated probe connected with a short glass "L" shape adaptor to four impingers in series. The first and second impingers were each charged with 100 ml. of deionized water. The third impinger was empty and the fourth impinger contained approximately 400 grams of indicating silica gel. A fiberglass filter was located between the third and fourth impingers and was operated at ambient temperature. Figure 2 is a diagram of the particulate matter sampling train.

FIGURE 2

WET IMPINGEMENT SAMPLING TRAIN FOR PARTICULATE MATTER



Three particulate matter trains were run for a period of 72 minutes each. The trains were leak checked prior to and at the conclusion of each run. The nozzle, probe, and glass adaptor were each rinsed with acetone and deionized water. The liquid gain in the impingers were determined. The liquids in the impingers were recovered and the impingers were rinsed with deionized water and acetone. The filter was recovered and placed in a tared petri dish, and the front half of the filter holder was rinsed with deionized water and acetone. The weight gain in the silica gel impinger was determined with an electronic scale Ohaus, Model #1500.

Analyses were performed both by ES and SDAPCD laboratories. One complete set of samples (Run #1, with blanks) was turned over to the SDAPCD for analysis. The rest of the samples (Run #2 and #3) were analyzed at the ES laboratory. Analysis involved the drydown of the nozzle-probe washes, liquid catch, and filter. An organic extraction with petroleum ether was performed on the liquid catch as specified by SDAPCD analytical procedures.

QUALITY ASSURANCE

The Quality Assurance procedures that were employed for this project were based on the guidelines published by the EPA in "Quality Assurance Handbooks for Air Pollution Measurement Systems", Volume III, EPA-600/4-77-0276.

Field Testing Quality Assurance

Prior to and at the conclusion of field sampling, each meter box dry gas meter and orifice was calibrated against a wet test meter. The results of orifice calibration were expressed as the delta H@ at various pressure drops (in inches of water) to achieve 0.75 CFM, as specified in EPA publication APTD-0576. The dry gas meter accuracy was expressed as gamma (Y) and was determined as the ratio between the meter box dry gas meter and the wet test meter.

Exhaust gas, filter, meter and impinger temperatures were monitored using a type-K thermocouple connected to an Omega Model 601 digital readout.

Exhaust gas velocity was determined for establishing isokinetic sampling rates and volumetric flow using an S-type pitot tube attached to the probe as specified in EPA Method 2.

At the conclusion of each test run the sampling train was leak checked at a vacuum equal to or greater than the highest vacuum observed during the test runs. Each sampling train was considered leak free since the leak rate was less than 0.02 CFM.

At the beginning of the field testing program, a probe wash and flexible line wash were obtained and identified as field blanks. The probe wash technique, all sampling and recovery reagents, sample containers and sample handling used for the test runs were identical to those used to obtain the field blanks.

Laboratory Quality Assurance

Filter drydown weights were obtained using an analytical balance. Prior to conducting weighings, the accuracy of the balance was checked with a 100 mg Class S weight. All weighings were conducted in an environmentally controlled balance room maintained at 70 °F, with a relative humidity of less than or equal to 50%. All samples were conditioned and desiccated before weighing and a constant weight was defined as ± 0.5 mg between consecutive weighings with an elapsed time between weighings greater than 6 hours. All weight data are recorded in a permanently bound notebook maintained in the balance room.

All reagents for charging the sample train and sample recovery were ACS reagent grade materials. ES participates in the EPA inter-laboratory quality assurance program.

Sample Custody

A specific Chain-of-Custody procedure was used for this project. The elements of this plan include:

- o Train component identification
- o Sample identification
- o Sample labels
- o Documentation
- o Chain of custody forms

The sequence of activities concerned with sample custody together with identification and tracking procedures are described below:

1. Sample train prepared by the laboratory including filter holders, impingers, and other sampling equipment identified by tags and codes.
2. Sample train issued to test team and master log filled out. Sample I.D. number stickers issued according to test identification code.

3. Train returned to recovery area when a valid sample is obtained. Sample train accompanied by all field data sheets.
4. Recovery team recovered samples using appropriate containers, affixed sample I.D. labels to sample containers, to master log, to field data sheet, and to train recovery sheet.
5. All samples returned to ES Pasadena laboratory with Chain-of-Custody form.
6. Samples transferred or shipped to appropriate laboratory with Chain-of-Custody form.
7. Samples examined at each transfer point for integrity (broken containers, loss in liquid, or seal integrity).

Upon completing the required analysis, the analyst returned the Chain-of-Custody form along with results to ES. All samples were accounted for by the ES laboratory supervisor and the project manager. Each laboratory identified samples in its own laboratory notebooks by the ES I.D. number as well as any internal identification. Notebooks are retained by each laboratory according to usual laboratory practices.

RESULTS

The results of the testing are presented in Tables 1 and 2. The samples from Run #1 and reagent/filter blanks were given to a representative of the SDAPCD. Data from Run #1 and the averages from all three runs are not included in the tables at the request of SDAPCD. Tables 3 and 4, are summaries of plant process data, and production rate. Supporting data and process calculations of the production rate were provided to ES by Andy Segal and Dean Carlson of SDAPCD and are included in the Appendix. Additional supporting data are located in the Appendix.

Table 1
Summary of Exhaust Gas Flow Data
Baghouse Exhaust Stack
Pala Asphalt Plant
Pala, California
December 12, 1990

Parameter	Results		
	Run 1	Run 2	Run 3
Time (hours)		1105-1222	1318-1439
Stack Temp. (°F)		204	193
Moisture (%)		19.6	22.2
Oxygen (%)		14.1	13.4
Carbon Dioxide (%)		4.5	5.5
Molecular Wt. (dry)		29.28	29.42
Molecular Wt. (wet)		27.19	26.88
Velocity (fps)		52.42	51.52
Flow			
ACFM		29,901	29,385
DSCFM		18,536	17,924

Note: 1) For all Run #1 data, please see SDAPCD report.

Table 2
Summary of Particulate Matter Flow Data
Baghouse Exhaust-Stack
Pala Asphalt Plant
Pala, California
December 12, 1990

Parameter		Results	
		Run 1	Run 3
Time (hours)		1105-1222	1318-1439
Front Half	(gr/DSCF)	0.0028	0.0026
	(gr/ACF)	0.0017	0.0016
	(lb/hr)	0.44	0.41
Back Half	(gr/DSCF)	0.0077	0.0072
	(gr/ACF)	0.0048	0.0044
	(lb/hr)	1.22	1.10
Total	(gr/DSCF)	0.0105	0.0098
	(gr/ACF)	0.0065	0.0060
	(lb/hr)	1.66	1.51

Note: 1) For all Run #1 data, please see SDAPCD report.
2) Particulates in organic fractions were less than 0.01 mg.

Table 3
Summary of Production and Operational Data
Baghouse Exhaust Stack
Pala Asphalt Plant
Pala, California
December 12, 1990

Production Results					
Time	Baghouse Delta P (inch water)	Material Temp. (°F)	Baghouse Inlet Temp (°F)	Damper Position (Deg.)	Exhaust Fan Ammeter (Amps)
0750	Start test/Production count.				
0830	4.8	291	230	62	85
0900	4.9	294	225	62	85
1020	4.9	293	228	65	85
1200	5.0	296	220	65	85
1430	4.9	294	212	66	85
1439	End test/Production count.				
1500	5.0	292	219	66	85
Average	4.9	294	223	64	85

Note: Baghouse inlet temperature operational limit was 275 °F. (Nomex bag material design limit is 420 °F. Production total time was 6.82 hrs (0750 to 1439).

Table 4
Summary of Batch Mix Type
Baghouse Exhaust Stack
Pala Asphalt Plant
Pala, California
December 12, 1990

Type	Batch Results				
	3/8" (lbs)	1/2" (lbs)	3/4" (lbs)	Berm (lbs)	Sheet (lbs)
Sand	1,146	908	778	1,138	1,816
3/8 rock	714	756	474	710	NA
1/2 rock	NA	209	380	NA	NA
3/4 rock	NA	NA	247	NA	NA
Filler	20	19	19	20	20
Oil AR 4000	120	108	102	NA	164
Oil AR 8000	NA	NA	NA	132	NA
Total	2,000	2,000	2,000	2,000	2,000

APPENDICES

APPENDIX A
FIELD DATA

Engineering-Science, Pasadena, California

Plant: Pala
Source: BH Stack
Date: 12/12/90
Run: 2 1105-1222
Standard Temp = 60 deg F Standard Press = 29.92 in Hg

FLOW DATA

STACK DIAMETER (inches)	41.75
STACK CROSS-SECTIONAL AREA (sq feet)	9.51
BAROMETRIC PRESSURE (inches Hg)	29.42
OXYGEN CONTENT (%)	14.1
CARBON DIOXIDE CONTENT (%)	4.5
MOISTURE CONTENT (%)	19.6
STACK TEMPERATURE (deg F)	204
STACK STATIC PRESSURE (inches water)	0.37
DRY STACK GAS MOLECULAR WEIGHT	29.28
VELOCITY PRESSURE (sq rt inches water)	0.80
PITOT TUBE CORRECTION FACTOR	0.84
VELOCITY (ft per sec)	52.42
EXHAUST GAS FLOW RATE (ACFM)	29,901
EXHAUST GAS FLOW RATE (DSCFM)	18,536

SAMPLING DATA

DRY GAS VOLUME SAMPLED (DCF)	48.509
DRY GAS VOLUME SAMPLED (DSCF)	45.989
DRY GAS METER TEMPERATURE (deg F)	76
DRY GAS METER GAMMA	0.99
AVERAGE ORIFICE PRESSURE (inches water)	1.55
TOTAL RUN TIME (min)	72
NOZZLE DIAMETER (inches)	0.250
ISOKINETIC (%)	96.3

LABORATORY DATA

MOISTURE RECOVERED (mls)	240.60
PARTIC. FROM NOZ., PROBE & WASHES (mg)	7.60
PARTICULATE FROM FILTER (mg)	0.70
PARTICULATE FROM IMPINGERS (mg)	22.90

PARTICULATE DATA

FRONT HALF (gr/DSCF)	0.0028
(gr/ACF)	0.0017
(lb/hr)	0.44
BACK HALF (gr/DSCF)	0.0077
(gr/ACF)	0.0048
(lb/hr)	1.22
TOTAL (gr/DSCF)	0.0105
(gr/ACF)	0.0065
(lb/hr)	1.66

Engineering-Science, Pasadena, California

Plant: Pala
 Source: BH Stack
 Date: 12-12-90
 Run: 3 PM 1318-1439
 Standard Temp = 60 deg F Standard Press = 29.92 in Hg

FLOW DATA

STACK DIAMETER (inches)	41.75
STACK CROSS-SECTIONAL AREA (sq feet)	9.51
BAROMETRIC PRESSURE (inches Hg)	29.42
OXYGEN CONTENT (%)	13.4
CARBON DIOXIDE CONTENT (%)	5.5
MOISTURE CONTENT (%)	22.2
STACK TEMPERATURE (deg F)	193
STACK STATIC PRESSURE (inches water)	0.37
DRY STACK GAS MOLECULAR WEIGHT	29.42-
VELOCITY PRESSURE (sq rt inches water)	0.79
PITOT TUBE CORRECTION FACTOR	0.84
VELOCITY (ft per sec)	51.52-
EXHAUST GAS FLOW RATE (ACFM)	29,385-
EXHAUST GAS FLOW RATE (DSCFM)	17,924-

SAMPLING DATA

DRY GAS VOLUME SAMPLED (DCF)	46.476
DRY GAS VOLUME SAMPLED (DSCF)	44.556-
DRY GAS METER TEMPERATURE (deg F)	70
DRY GAS METER GAMMA	0.99
AVERAGE ORIFICE PRESSURE (inches water)	1.51
TOTAL RUN TIME (min)	72
NOZZLE DIAMETER (inches)	0.250
ISOKINETIC (%)	96.3-

LABORATORY DATA

MOISTURE RECOVERED (mls)	272.90
PARTIC. FROM NOZ., PROBE & WASHES (mg)	7.60
PARTICULATE FROM FILTER (mg)	0.01
PARTICULATE FROM IMPINGERS (mg)	20.70

PARTICULATE DATA

FRONT HALF (gr/DSCF)	0.0026
(gr/ACF)	0.0016
(lb/hr)	0.41
BACK HALF (gr/DSCF)	0.0072
(gr/ACF)	0.0044
(lb/hr)	1.10
TOTAL (gr/DSCF)	0.0098
(gr/ACF)	0.0060
(lb/hr)	1.51

၆၂

Particulate
matter

$$K = 2.4$$

餅

Plant CAC MA7 P4CA

03-21-90

West Site Stock on file

Run Number #2, 2.14.

operator AJN, V-3

270

Ambient Temp 70
Barometer 29.67

Barometric 29.72
stack pressure + 3.2

Stack 1120 & 70

stack Dia 41.75

Meyer 110 1.983

Hotel Gamma - 785

Meter Box ! Group II

Nozzle Diameter $\frac{1}{8}$ in.

Probe Length 5 1/2 ft

Probe Mat'l Overlaid

Filter Number 091146

Sample Box 1

PRE LEAK 0.014 w/s

POST-DEAK PRAY. IMPROV.

Run Number <u>AN-05</u>		Stack Dia <u>41.75</u>		Probe Length <u>5 1/2 ft</u>		TEMPERATURES										FUP VAC. "Hg
TRAVERSE POINT NUMBER	ELAPSED TIME (mins)	CLOCK TIME	GAS METER READING (Vn)	VELOCITY HEAD (delta p)	ORIFICE PRESSURE (delta H, "H ₂ O)		STACK (T _s)	METER INLET	METER OUT	IMPINGER	FILTER					
					Desired	Actual										
1	6	1105	983.290	.55	1.32	1.3	217	85	83	63	N/A		3			
2	7	1108	985.3	.61	1.46	1.5	24	80	79	60			3			
3	6	1111	987.3	.69	1.66	1.7	240	81	79	56			3			
4	9	1114	989.3	.74	1.77	1.8	240	81	79	54			3			
5	12	1117	991.5	.73	1.75	1.8	209	81	78	51			3			
6	15	1120	993.7	.74	1.77	1.8	207	80	77	49			4			
7	18	1123	996.0	.68	1.63	1.6	203	79	76	49			3			
8	21	1126	998.0	.62	1.49	1.5	201	77	76	51			3			
9	24	1129	000.0	.60	1.44	1.4	199	77	75	51			3			
10	27	1132	002.0	.57	1.37	1.4	197	77	74	52			3			
11	30	1135	003.9	.59	1.42	1.4	197	77	74	53			3			
12	33	1138	5.8	.53	1.27	1.3	199	77	75	54			3			
	36	1141	7.681		port	Merry										
AVERAGE /SUM																

UN
W

W.D.M.

$$k = 2.4$$

Probe Mat'l Quartz
Filter Number 091146
Samp Box 1 —
PRE LEAK 0.003
POST. LEAK 0.002 @ 15" Hg

Meter #110 1982
Meter Gamma 985
Meter Box 1 Down II
Nozzle Diameter .2487 in
Probe Length 5 1/2 ft

Ambient Temp 70°
Barometer 29.92
Stack Pressure 1.37
stack 120 10%
stack Dia 41.75"

Plant CAL MA7 PXA
Date 12-12-80
Test Site Stack Outlet
Run Number # 3 J.M.
Operator P.J. N.J.

[illegible]

ES

ENGINEERING-SCIENCE
COMPANIES

add 36 inches
to each

4:17 PM

$\tau = 2.4$

Plant Cal-Mat - Delo

Date 12-15-90

POST LEAK RATE: 0.002015" Hg

Page 2 of 2
Run Number 5
Operator S. S. Medina

1.000 @ 15" Hg

TRAVERSE POINT NUMBER	ELAPSED TIME (mins)	CLOCK TIME	GAS METER READING (V _m)	VELOCITY HEAD (delta p)	ORIFICE PRESSURE (delta H, "H ₂ O)		TEMPERATURES				PUMP VAC. "Hg	
					Desired	Actual	STACK - (T _e)	METER INLET	METER OUT	IMPINGER	FILTER	
1	0	1404	55.035	0.51	1.22	1.2	189	68	67	55	N/A	8
2	3	1407	56.8	0.58	1.39	1.4	190	70	68	52		10
3	6	1410	58.6	0.56	1.34	1.3	191	72	68	50		10
4	9	1413	60.5	0.57	1.37	1.4	192	72	68	50		12
5	12	1416	62.3	0.55	1.32	1.3	191	73	69	51		10
6	15	1419	64.1	0.61	1.46	1.5	194	73	69	53		13
7	18	1422	66.1	0.67	1.61	1.6	195	74	69	54		13
8	21	1425	68.1	0.72	1.73	1.7	196	73	69	54		15
9	24	1428	70.0	0.72	1.73	1.7	195	73	68	55		16
10	27	1431	72.1	0.77	1.85	1.9	194	73	69	56		20
11	30	1433	74.3	0.78	1.85	1.8	194	72	69	55		20
12	33	1436	76.4	0.63	1.51	1.5	193	72	69	55		15
	36	1439	78.353	END TEST								
AVERAGE /SUM	72		46.476	0.79		1.51	193	70				

PRELIMINARY VELOCITY TRAVERSE DATA

PRELIMINARY VELOCITY TRAVERSE DATA

Plant Calmat @ P.A.C.A. Date 12/12/98

Location B.H. stack outlet Stack I.D. 41.75"

Barometric Pressure _____ Static Pres 0.37 "H₂O

Operators MN, O.P.

TRAVERSE POINT NUMBER	VELOCITY HEAD	STACK TEMP.	CYCLONIC FLOW ANGLE
1	0.44	135	20
2	0.56	140	11
3	0.58	140	18
4	0.55	142	17
5	0.57	143	20
6	0.56	144	18
7	0.56	144	15
8	0.58	145	13
9	0.65	147	15
10	0.63	136	15
11	0.58	135	15
12	0.55	131	17
AVERAGE			

TRAVERSE POINT NUMBER	VELOCITY HEAD	STACK TEMP.	CYCLONIC FLOW ANGLE
1	0.59	130	17
2	0.65	135	17
3	0.76	140	17
4	0.76	141	16
5	0.71	145	16
6	0.68	143	11
7	0.66	143	17
8	0.61	145	15
9	0.65	142	11
10	0.62	140	9
11	0.56	140	9
12	0.51	135	10
AVERAGE	NAP	140	14.96

APPENDIX B
LAB DATA

Project No.:

WAZO:

Date Analyzed:

12/17/90

Technician:

Clarín

Project Name:

77A

57A

[illegible]

TRAIN RECOVERY SHEET

Date 12/13/91
 Facility PAZA
 Technician DMB

Run # 1 Method # 5.1
 Type PM
 Imp. Solution H₂O

	Solution	Vol. (ml)	Volume Marked?	
Nozzle- Probe Rinse				
Umbilical Rinse				
		Final (ml)	Initial (ml)	Net (ml)
Impinger # <u>1</u>	<u>H₂O</u>	<u>280.5</u>	<u>100</u>	<u>180.5</u>
Impinger # <u>2</u>	<u>H₂O</u>	<u>135.5</u>	<u>100</u>	<u>35.5</u>
Impinger # <u>3</u>	<u>MT</u>	<u>12</u>	<u>0</u>	<u>12.0</u>
Description				
Impinger Rinse				
		Final (g)	Initial (g)	
Silica Gel (Description)		<u>826.9</u>	<u>798.2</u>	<u>28.7</u>
Filter # (Description)		Total Moisture		<u>256.7 ml</u>
Field Blanks				
Disposition/Comments				

DATE 12/13/90TRAIN RECOVERY SHEET
E.S.# 9012148RUN# 2 METHOD 5.1TYPE PMIMP. SOLUTION H₂OFACILITY PALATECHNICIAN PM

NOZZLE-PROBE RINSE

~~EMERGENCY RINSE~~
~~noy - probe rinse~~IMPINGER # 1IMPINGER # 2IMPINGER # 3IMPINGER # /

DESCRIPTION

IMPINGER RINSE

SILICA GEL
(DESCRIPTION)FILTER# 091146
(DESCRIPTION)

FIELD BLANKS

~~probe rinse work:~~

DISPOSITION/COMMENTS

imp work: H₂O : 350 mlauton: 350 ml.

SOLUTION	VOL. (ml)	DESCRIPTION
<u>H₂O</u>	<u>350.5</u>	
<u>auton</u>	<u>105</u>	

	FINAL (ml)	INITIAL (ml)	NET (ml)
<u>H₂O</u>	<u>275</u>	<u>100</u>	<u>175</u>
<u>H₂O</u>	<u>133</u>	<u>100</u>	<u>33</u>
<u>MT</u>	<u>8</u>	<u>0</u>	<u>8</u>

	FINAL (g)	INITIAL (g)	
	<u>881.8</u>	<u>857.2</u>	<u>24.6</u>

TOTAL MOISTURE

240.6_(g)

DATE 12-13-90

TRAIN RECOVERY SHEET

RUN# 3 METHOD 5.1FACILITY PaiaE.S. # 9012149TYPE P.M.TECHNICIAN R.O.IMP. SOLUTION H₂O

NOZZLE-PROBE RINSE

UMBILICAL RINSE

SOLUTION	VOL. (ml)	DESCRIPTION

IMPINGER # 1IMPINGER # 2IMPINGER # 3IMPINGER #

DESCRIPTION

IMPINGER RINSE

	FINAL (ml)	INITIAL (ml)	NET (ml)
H ₂ O	325	100	225
H ₂ O	120	100	20
M+	5	0	5

SILICA GEL
(DESCRIPTION)

	FINAL (g)	INITIAL (g)	
	861.0	838.1	22.9

FILTER#
(DESCRIPTION)

	TOTAL MOISTURE

FIELD BLANKS

272.9 (g)

DISPOSITION/COMMENTS

DRY MOLECULAR WEIGHT DETERMINATION

PLANT Palo Alto Calmet
 DATE 12/12/90 analyzed 12/14/90
 SAMPLING TIME (24-hr CLOCK)
 SAMPLING LOCATION Bay Area stack south
 SAMPLE TYPE (BAG, INTEGRATED, CONTINUOUS) tidler bags
 ANALYTICAL METHOD Orsat W. 3
 AMBIENT TEMPERATURE 75-80 °F
 OPERATOR HSD & PDB

COMMENTS: Run #1

RUN GAS	1		2		3		AVERAGE NET VOLUME	MULTIPLIER	MOLECULAR WEIGHT OF STACK GAS (DRY BASIS) M _D , lb/lb-mole
	ACTUAL READING	NET	ACTUAL READING	NET	ACTUAL READING	NET			
CO ₂	5.2	5.2	5.4	5.4	5.2	5.2	5.3	44/100	
O ₂ (NET IS ACTUAL O ₂ READING MINUS ACTUAL CO ₂ READING)	19.0	13.8	19	13.6	19.0	13.8	13.7	32/100	
CO (NET IS ACTUAL CO READING MINUS ACTUAL O ₂ READING)								28/100	
N ₂ (NET IS 100 MINUS ACTUAL CO READING)								28/100	
TOTAL									

DRY MOLECULAR WEIGHT DETERMINATION

PLANT Pala Calicut
 DATE 12/12/90 analyzed 12/14/90
 SAMPLING TIME (24-hr CLOCK) _____
 SAMPLING LOCATION off stack outlet
 SAMPLE TYPE (BAG, INTEGRATED, CONTINUOUS) tidler bags
 ANALYTICAL METHOD gravimetric m: 3
 AMBIENT TEMPERATURE 75-80 °F
 OPERATOR HSD & JDB

COMMENTS:

Run #2

RUN GAS	1		2		3		AVERAGE NET VOLUME	MULTIPLIER	MOLECULAR WEIGHT OF STACK GAS (DRY BASIS) M _d , lb/lb-mole
	ACTUAL READING	NET	ACTUAL READING	NET	ACTUAL READING	NET			
CO ₂	4.6	4.6	4.4	4.4	4.6	4.6	44.5	44/100	
O ₂ (NET IS ACTUAL O ₂ READING MINUS ACTUAL CO ₂ READING)	17.8	13.2	18.8	14.4	19.2	14.6	14.1	32/100	
CO (NET IS ACTUAL CO READING MINUS ACTUAL O ₂ READING)								28/100	
N ₂ (NET IS 100 MINUS ACTUAL CO READING)								28/100	
TOTAL									

DRY MOLECULAR WEIGHT DETERMINATION

PLANT Palo Alto Calumet
 DATE 12/12/90 analyzed 12/14/90
 SAMPLING TIME (24-hr CLOCK) _____
 SAMPLING LOCATION Bay View stack outlet
 SAMPLE TYPE (BAG, INTEGRATED, CONTINUOUS) tidal bag
 ANALYTICAL METHOD anal M-3
 AMBIENT TEMPERATURE 75 - 80 °F
 OPERATOR HSD - DAB

COMMENTS:

Run # 3

RUN GAS	1		2		3		AVERAGE NET VOLUME	MULTIPLIER	MOLECULAR WEIGHT OF STACK GAS (DRY BASIS) M_d , lb/lb-mole
	ACTUAL READING	NET	ACTUAL READING	NET	ACTUAL READING	NET			
CO ₂	5.5	5.5	5.4	5.4	5.5	5.5	5.5	44/100	
O ₂ (NET IS ACTUAL O ₂ READING MINUS ACTUAL CO ₂ READING)	18.8	13.3	19.0	13.6	18.8	13.3	13.4	32/100	
CO (NET IS ACTUAL CO READING MINUS ACTUAL O ₂ READING)								28/100	
N ₂ (NET IS 100 MINUS ACTUAL CO READING)								28/100	
TOTAL									

APPENDIX C
QUALITY ASSURANCE
AND CALIBRATIONS

ENGINEERING SCIENCE
Pasadena, California

POST TEST METER BOX CALIBRATION FORM

Meter Box No. BROWN II Date 01-11-91 Calibrated by D MARSDEN

Barometric Pressure 29.85 Ambient Temp 65 Pre Test Y_1 0.985

Project Name PALA Project No. WA220 Hum 1.9 Vac 20

Orifice Manometer (in. H ₂ O) H	Gas Volume		Temperatures		Time (min) T _i	Y _i	H ₂
	Wet Test Meter (ft ³) V _w	Dry Gas Meter (ft ³) V _d	Wet Test Meter (° F) T _w	Dry Gas Meter (° F) T _d			
1.9	10.493	10.467	65	67	14	1.001	—
1.9	11.171	11.207	65	68	15	0.997	—
1.9	11.113	11.145	64	69	15	1.002	—
						Y _i AVG	1.000

METER BOX CALIBRATION HISTORY

Last Calibration Date 10-03-90 Calibrated by D MARSDEN

H₂ of Calibration 1.98 Y_i of Calibration 0.985

ENGINEERING SCIENCE
Pasadena, California

SOURCE SAMPLING NOZZLE CALIBRATION

Project No. WA 220 Date 11-02-90.
Calibrated by Q/A 2/2 Instrument BAUSHARPE DIGICAL.TC

Nozzle Number	Nominal Size	Reading Number			Average
		1	2	3	
140	$\frac{1}{8}$	.126	.127	.128	.127
186	$\frac{1}{8}$	.125	.126	.126	.1257
180	$\frac{3}{16}$	.1855	.1845	.186	.1853.
143.	$\frac{1}{8}$	.127	.127	.128	.1273.
177	$\frac{3}{16}$	.182	.183	.183	.1827
185	$\frac{1}{8}$	.1285	.1275	.128	.128
304	$\frac{1}{8}$	.1285	.1275	.1285	.1278.
178.	$\frac{3}{16}$	.178	.1775	.1775	.1778
ES 21	$\frac{3}{16}$	.179	.178	.178	.1783.
157	$\frac{1}{4}$	.249	.250	.250	.2497
98	$\frac{1}{4}$	.240	.241	.241	.2407
152	$\frac{5}{16}$	.301	.300	.300	.300
	$\frac{1}{4}$	.25	.25	.249	.2497

SPALA

~~XX~~

SOURCE TEST OF PARTICULATE EMISSIONS TO THE ATMOSPHERE

TEST SITE: Calmat-Pala
Pala Indian Reservation
Pala, CA 92059

ERRATA

TEST #: 91301

P.O.# 117

TEST DATE: 10/28/91

Type of plant (Asphalt / Perlite / Combustion):

asphalt

UNIT TESTED: Asphalt plant

EQUIPMENT: baghouse

TESTED BY: David Shina, Linda Twaddle, Gary Smith, & Andy Fuchs

DATE: 10/28/91

SITE PERSONNEL: Paul Mason

DATE: 10/28/91

APCD ENGINEER: Earnest Davis

DATE: 10/28/91

LAB ANALYSIS BY: David Shina

DATE: 11/6/91

REPORT BY: David Shina

DATE: 11/6/91

REVIEWED BY: Linda Twaddle

DATE:

APPROVED BY:

DATE:

ROBERT YELENOSKY, ACTING SENIOR AIR POLLUTION CHEMIST

This report has been reviewed and found to be representative of the testing that was performed.

TEST	PERMIT LIMIT	MEASURED	PERFORMANCE
RULE 54 DUST & FUMES	40 lbs/hr	4.03 lbs/hr	PASSED

SUMMARY:

ITEM	Vm	Bws	Cs	E	I	Qstd	ts	PROD RATE
UNITS	ft ³	%	gr/dscf	lbs/hr	%	dscfm	°F	tons/hr
VALUE	51.167	31.27	0.035	4.031	108	1.34E+04	248	240.50

SYSTEM DESCRIPTION:

This asphalt plant combines crushed rock and sand with asphalt oil in batch loads of varying sizes. The rock and sand are heated in a rotary drum to dry them. The exhaust from this dryer is routed through a baghouse and finally to a stack. It is the emissions from this stack that are the subject of this report.

PROCEDURES:

The procedures and equipment utilized in these tests are based on EPA New Source Performance Standards Method 5. The sampling train was modified to utilize a back-end filter and 5th impinger filled with silica gel (fig. 1), as outlined by the SDAPCD QA manual.

CALCULATIONS

All preliminary assumptions and calculations are based on data obtained from previous tests. All equations are from EPA CFR 40, July 1, 1990, Parts 53-60, Appendix A, Methods 1-5 inclusive.

PARTICULATE SAMPLING:

The test consisted of sampling at 24 traverse points, 12 from each of 2 sample ports (fig.2), collected from 77 inches below the stack (fig.3). All field data was transferred to the computer printout. All calculations were done by the computer and the emissions were compared to rule 54 of the SDAPCD.

ANALYSES:

Gas: An integrated bag sample was collected during the test and analyzed at the APCD lab.

Particulate: All procedures follow EPA guidelines, except where noted in the SDAPCD QA manual.

EQUIPMENT:

All testing and analysis equipment was calibrated according to EPA guidelines.

Analysis:

Collection:

Sampling:

Temp./Press.:

CO2-Anarad AR400
O2-Teledyne Ryan 320 P4
Macrobalance-Sargent Welch
Microbalance-Sartorius
ver.4 APCD P/M-ISOS 9/10/91 by DNS

Filter-Gelman
Holder-Gelman
Beakers-Pyrex
Impingers-Ace

L/S Box-Napp
Umbilical cord-Napp
Cold/Hot box-Napp
Pitot tube-Napp
Thermocouples-Omega
Read out-Omega
Barometric-calc. by APCD
L/S box-Dwyer magnehelic

Printed: 12/12/91 @ 1:18 PM Page 1 of 3

Trav. Pt	Vm (ft ³)	ΔP	ΔH	t 1(unc)	t 2(unc)	Stack Temp	Imp Temp	velocity
	506.861	(in H ₂ O)	(in H ₂ O)	(°F)	(°F)	(°F)	(°F)	(ft/sec)
†† East 12		0.350	2.700	66.00	82.00	247.00	50	41.34
11		0.350	2.700	64.00	84.00	249.00	48	41.40
10		0.390	3.000	65.50	98.00	254.00	48	43.86
9		0.420	3.200	66.00	100.00	254.00	51	45.51
8		0.450	3.500	67.00	102.00	256.00	56	47.18
7		0.470	3.600	67.00	104.00	258.00	58	48.28
6		0.520	4.000	68.00	105.00	259.00		50.82
5		0.520	4.000	69.00	106.00	260.00	61	50.86
4		0.510	3.900	69.50	107.00	258.00	59	50.29
3		0.520	4.000	70.00	108.00	255.00	56	50.68
2		0.470	3.600	70.00	108.00	256.00	55	48.18
East 1		0.470	3.600	71.00	109.00	254.00	54	48.15
South 12		0.250	1.900	74.00	71.00	149.00	53	32.43
11		0.370	2.900	74.00	102.00	190.00	48	40.76
10		0.420	3.200	73.00	106.00	242.00	47	45.13
9		0.450	3.500	73.00	108.00	259.00	46	47.28
8		0.500	3.900	74.00	110.00	260.00	47	49.87
7		0.500	3.900	74.00	110.00	261.00	47	49.90
6		0.510	3.900	74.00	111.00	260.00	48	50.36
5		0.510	3.900	75.00	112.00	258.00	48	50.29
4		0.480	3.700	75.50	113.00	258.00	46	48.79
3		0.430	3.300	76.00	114.00	257.00	50	46.15
2		0.460	3.500	77.00	114.50	268.00	50	47.70
South 1	558.028	0.430	3.300	78.00	116.00	253.00	51	46.02

	Vm (ft ³)	ΔP (in H ₂ O)	ΔH (in H ₂ O)	t 1 (°F)	t 2 (°F)	ts (°F)	ti (°F)	vs (ft/sec)
Average:	51.167	0.445	3.446	71.27	104.19	248	51	46.72

MISCELLANEOUS:

Ø = 60.0 min
 tn = 24 points
 α = 2.5 min

NOZZLE & PROBE:

Dn = 0.310 in
 An = 0.0755 in²
 Cp = 0.846

METER BOX PARAMETERS:

ΔH@ = 2.7254
 Y = 0.9782
 Box ID = D-337

PRESSURES:

Pbar = 29.46 in Hg
 Pg = -0.38 in H₂O
 Silica gel(yes/no) = yes
 Vpw @ ts = 58.63 in Hg
 Vpw @ ti = 0.0000 in Hg

VOLUME:

start leak rate = 0.010 cfm
 Pass/Fail PASS
 final leak rate = 0.000 cfm
 Pass/Fail PASS
 Vm = 51.167 ft³

TEMPERATURES:

t1 corr = 0.40 °F
 t2 corr = 0.10 °F
 tm = 88 °F
 ts = 248 °F
 ti = 51 °F

STACK PARAMETERS:

circular (yes/no) = yes
 Ds = 3.48 ft
 Length = N/A ft
 As = 9.51 ft²

LAB DATA:

mn(front) = 0.02492 g
 mn(back) = 0.08385 g
 mn(total) = 0.10877 g
 Vlc = 461.69 ml

STACK GAS MEASUREMENTS:

CO₂ = 3.20 %
 O₂ = 17.40 %
 CO = 0.00 %
 N₂ = 79.40 %

†† The stack has 2-5 inch ports, so we had to adapt a impinger train support at the site, because we do not have 5"-3" scale down uniraill port adapters. Our impinger train support forced me to combine points 12 & 11 on the east port. We could sample all the points on the south port.

TEMPERATURES:

01)	$ts = (\sum ts(n))/total\ n's$	248 °F
02)	$Ts = ts + 460$	708 °R
03)	$tm = (\sum \{(t_1(n) + t_2(n))/2\})/total\ n's$	88 °F
04)	$Tm = (t_1 + t_2)/2 + 460$	548 °R
05)	$ti = (\sum ti(n))/total\ n's$	51 °F
06)	$Tstd$	528 °R

PRESSURES:

07)	$Pbar = \{(P @ S.L.) + [ft. above S.L. * (-0.1 in Hg/100ft)]\}$	29.46 in Hg
08)	$Pg = \text{read from pressure sensing device}$	-0.38 in H ₂ O
09)	$Ps = Pbar + (Pg/13.6)$	29.43 in Hg
10)	ΔH	3.45 in H ₂ O
11)	$Pm = Pbar + (\Delta H/13.6)$	29.71 in Hg
12)	$Pstd$	29.92 in Hg

VOLUME:

13)	$Vm = Vm(end) - Vm(begin)$	51.167 ft ³
14)	Y	0.9782
15)	$Vm' = Vm * Y$	50.052 ft ³
16)	$Vpw @ ti = \text{from appendix}$	0.0000
17)	$corr\ Vwm = \{[(Vm' * Vpw @ imp / Ps) * Pm * Tstd] / (Tm * Pstd)\}$	0.0000 ft ³
18)	$Vm\ std = \{[Vm' * (Tstd / Tm) * (Pm / Pstd)] - corr\ Vwm\}$	47.894 ft ³
19)	$Vlc = (\sum \text{Volume of impingers})$	461.69 ml
20)	∂	0.002201 lb/ml
21)	R	21.85 Hg-ft ³ /°R-lb-mo
22)	MwH_2O	18.00 g/g-mo
23)	$Vw\ std = \{[(Vlc * \partial * R * Tstd) / (Pstd * MwH_2O)] + corr\ Vwm\}$	21.7918 ft ³

CALCULATIONS:**MOISTURE-**

24)	$Bws(1) = (Vw\ std) / (Vw\ std + Vm\ std) * 100$	31.27 %
25)	$Vpw @ ts = \text{from appendix}$	58.63 in Hg
26)	$Bws(2) = [(Vpw @ ts) / Ps] * 100$	199.20 %
27)	$Bws = \text{lower value of equation 24 or 26}$	31.27 %

MOLECULAR WEIGHT-

28)	$\%O_2$	17.40 %
29)	$\%CO_2$	3.20 %
30)	$\%N_2 + \text{inerts} + \%CO$	79.40 %
31)	$Md = [0.440(\%CO_2)] + [0.320(\%O_2)] + [0.280(\%N_2 + \text{inerts} + \%CO)]$	29.21 g/g*mole
32)	$Ms = Md * (1 - Bws) + 18.0 * (Bws)$	25.70 g/g*mole

FLOW-

33)	ΔP	0.445 in H ₂ O
34)	Cp	0.846
35)	$vs = 85.49 * Cp * [(Ts * \Delta P) / (Ps * Ms)]^{.5}$	46.719 ft/s
36)	$As = 3.14 * [(Ds)^2 / 4]$	9.51 ft ²
37)	$Qs = (vs) * As * 60$	2.66E+04 acfm
38)	$Qstd = 17.64 * Qs * (1 - Bws) * Ps / Ts$	1.34E+04 dscfm

EMISSIONS-**FRONT HALF**

39)	$mn\ (front)$	0.02492 g
40)	$Cs\ (front) = 15.43 * mn(front) / Vm\ std$	0.0080 0.008 grains/dscf
41)	$E\ (front) = (0.00857) * (Qstd) * Cs\ (front)$	0.92 lbs/hr

BACK HALF

42)	$mn\ (back)$	0.08385 g
43)	$Cs\ (back) = 15.43 * mn(back) / Vm\ std$	0.0270 0.027 grains/dscf
44)	$E\ (back) = (0.00857) * (Qstd) * Cs\ (back)$	3.11 lbs/hr

TOTAL

45)	$mn\ (total) = mn(front) + mn(back)$	0.10877 g
46)	$Cs\ (total) = 15.43 * mn(total) / Vm\ std$	0.0350 0.035 grains/dscf
47)	$E\ (total) = (0.00857) * (Qstd) * Cs\ (total)$	4.03 lbs/hr

ISOKINETICS:

48)	$An = 3.14 * [(Dn)^2 / 4]$	0.0755 in ²
49)	$I = .09450 * (Ts * Vm\ std) / Ps * vs * An * \partial * (1 - Bws)$	107.88 % = 108 %

Calmat-Pala on 10/28/91 P.O.#117 TEST #
 SAN DIEGO AIR POLLUTION CONTROL DISTRICT, 9150 CHESAPEAKE DRIVE, SAN DIEGO, CA, 92123

SOURCE TEST OF PARTICULATE EMISSIONS TO THE ATMOSPHERE

TEST SITE: Calmat-Pala
 Pala Indian Reservation
 Pala, CA 92059

TEST #: 91301

P.O.# 117

TEST DATE: 10/28/91

Type of plant (Asphalt / Perlite / Combustion):

asphalt

UNIT TESTED: Asphalt plant

EQUIPMENT: baghouse

TESTED BY: David Shina, Linda Twaddle, Gary Smith, & Andy Fuchs

DATE: 10/28/91

SITE PERSONNEL: Paul Mason

DATE: 10/28/91

APCD ENGINEER: Earnest Davis

DATE: 10/28/91

LAB ANALYSIS BY: David Shina

DATE: 11/6/91

REPORT BY: David Shina

DATE: 11/6/91

REVIEWED BY: Linda Twaddle

DATE: 11/21/91

APPROVED BY:

DATE: 11/26/91

ROBERT YELENOSKY, ACTING SENIOR AIR POLLUTION CHEMIST

This report has been reviewed and found to be representative of the testing that was performed.

TEST	PERMIT LIMIT	MEASURED	PERFORMANCE
RULE 54 DUST & FUMES	40 lbs/hr	4.03 lbs/hr	PASSED

SUMMARY:

ITEM	Vm	Bws	Cs	E	I	Qstd	ts	PROD RATE
UNITS	ft ³	%	gr/dscf	lbs/hr	%	dscfm	°F	tons/hr
VALUE	51.167	31.27	0.035	4.031	108	1.34E+04	248	240.50

SYSTEM DESCRIPTION:

This asphalt plant combines crushed rock and sand with asphalt oil in batch loads of varying sizes. The rock and sand are heated in a rotary drum to dry them. The exhaust from this dryer is routed through a baghouse and finally to a stack. It is the emissions from this stack that are the subject of this report.

PROCEDURES:

The procedures and equipment utilized in these tests are based on EPA New Source Performance Standards Method 5. The sampling train was modified to utilize a back-end filter and 5th Impinger filled with silica gel (fig. 1), as outlined by the SDAPCD QA manual.

CALCULATIONS

All preliminary assumptions and calculations are based on data obtained from previous tests. All equations are from EPA CFR 40, July 1, 1990, Parts 53-60, Appendix A, Methods 1-5 inclusive.

PARTICULATE SAMPLING:

The test consisted of sampling at 24 traverse points, 12 from each of 2 sample ports (fig.2), collected from 77 inches below the stack (fig.3). All field data was transferred to the computer printout. All calculations were done by the computer and the emissions were compared to rule 54 of the SDAPCD.

ANALYSES:

Gas: An integrated bag sample was collected during the test and analyzed at the APCD lab.

Particulate: All procedures follow EPA guidelines, except where noted in the SDAPCD QA manual.

EQUIPMENT:

All testing and analysis equipment was calibrated according to EPA guidelines.

Analysis:

CO2-Anarad AR400
 O2-Teledyne Ryan 320 P4
 Microbalance-Sargent Welch
 Microbalance-Sartorius

Collection:

Filter-Gelman
 Holder-Gelman
 Beakers-Pyrex
 Impingers-Ace

Sampling:

L/S Box-Napp
 Umbilical cord-Napp
 Cold/Hot box-Napp
 Pitot tube-Napp

Temp./Press.:

Thermocouples-Omega
 Read out-Omega
 Barometric-calc. by APCD
 L/S box-Dwyer magnehelic

ver.4 APCD P/M-ISOS 9/10/91 by DNS

Printed: 11/21/91 @ 8:33 AM Page 1 of 3

Calmat-Pala on 10/28/91

P.O.#117 TEST #91301

Trav. Pt	Vm (ft ³)	ΔP	ΔH	t 1(unc)	t 2(unc)	Stack Temp	Imp Temp	velocity
	506.861	(in H ₂ O)	(in H ₂ O)	(°F)	(°F)	(°F)	(°F)	(ft/sec)
†† East 12		0.350	2.700	66.00	82.00	247.00	50	41.34
11		0.350	2.700	64.00	84.00	249.00	48	41.40
10		0.390	3.000	66.50	88.00	254.00	48	43.86
9		0.420	3.200	66.00	100.00	254.00	51	45.51
8		0.450	3.500	67.00	102.00	256.00	56	47.18
7		0.470	3.600	67.00	104.00	258.00	58	48.28
6		0.520	4.000	68.00	105.00	259.00		50.82
5		0.520	4.000	69.00	106.00	260.00	61	50.86
4		0.510	3.900	69.50	107.00	258.00	59	50.29
3		0.520	4.000	70.00	108.00	255.00	56	50.68
2		0.470	3.600	70.00	108.00	255.00	55	48.18
East 1		0.470	3.600	71.00	109.00	254.00	54	48.15
South 12		0.250	1.900	74.00	71.00	149.00	53	32.43
11		0.370	2.900	74.00	102.00	190.00	48	40.76
10		0.420	3.200	73.00	106.00	242.00	47	45.13
9		0.450	3.500	73.00	108.00	259.00	46	47.28
8		0.500	3.900	74.00	110.00	260.00	47	49.87
7		0.500	3.900	74.00	110.00	261.00	47	49.90
6		0.510	3.900	74.00	111.00	260.00	48	50.38
5		0.510	3.900	75.00	112.00	258.00	48	50.29
4		0.480	3.700	75.50	113.00	258.00	48	48.79
3		0.430	3.300	76.00	114.00	257.00	50	46.15
2		0.460	3.500	77.00	114.50	256.00	50	47.70
South 1	558.028	0.430	3.300	78.00	116.00	253.00	51	46.02

	Vm (ft ³)	ΔP (in H ₂ O)	ΔH (in H ₂ O)	t 1 (°F)	t 2 (°F)	ts (°F)	ti (°F)	vs (ft/sec)
Average:	51.167	0.445	3.446	71.27	104.19	248	51	46.72

MISCELLANEOUS:

Ø = 60.0 min
 tn = 24 points
 ø = 2.5 min

NOZZLE & PROBE:

Dn = 0.310 in
 An = 0.0755 in²
 Cp = 0.846

METER BOX PARAMETERS:

ΔH@ = 2.7254
 Y = 0.9782
 Box ID = D-337

PRESSURES:

Pbar = 29.46 in Hg
 Pg = -0.38 in H₂O
 Silica gel(yes/no) = yes
 Vpw @ ts = 58.63 in Hg
 Vpw @ ti = 0.0000 in Hg

VOLUME:

start leak rate = 0.010 cfm
 Pass/Fail PASS
 final leak rate = 0.000 cfm
 Pass/Fail PASS
 Vm 51.167 ft³

TEMPERATURES:

t1 corr = 0.40 °F
 t2 corr = 0.10 °F
 tm = 88 °F
 ts = 248 °F
 ti = 51 °F

STACK PARAMETERS:

circular (yes/no) = yes
 Ds = 3.48 ft
 Length = N/A ft
 As = 9.51 ft²

LAB DATA:

mn(front) = 0.02492 g
 mn(back) = 0.08385 g
 mn(total) = 0.10877 g
 Vlc 461.69 ml

STACK GAS MEASUREMENTS:

CO₂ = 3.20 %
 O₂ = 17.40 %
 CO = 0.00 %
 N₂ = 79.40 %

†† The stack has 2-5 inch ports, so we had to adapt a impinger train support at the site, because we do not have 5"-3" scale down untrail port adapters. Our impinger train support forced me to combine points 12 & 11 on the east port. We could sample all the points on the south port.

Calmat-Pala on 10/28/91

P.O.#117 TEST #91301

TEMPERATURES:

01)	$ts = (\sum ts(n))/total\ n's$	248 °F
02)	$Ts = ts+460$	708 °R
03)	$tm = (\sum \{(t1(n)+t2(n))/2\}/total\ n's$	88 °F
04)	$Tm = (t1+t2)/2 + 460$	548 °R
05)	$ti = (\sum ti(n))/total\ n's$	51 °F
06)	$Tstd$	528 °R

PRESSURES:

07)	$Pbar = \{(P @ S.L.) + \{ft. above S.L. \cdot (-0.1 in. Hg/100ft)\}\}$	29.46 in Hg
08)	$Pg =$ read from pressure sensing device	-0.38 in H2O
09)	$Ps = Pbar + (Pg/13.6)$	29.43 in Hg
10)	ΔH	3.45 in H2O
11)	$Pm = Pbar + (\Delta H/13.6)$	29.71 in Hg
12)	$Pstd$	29.92 in Hg

VOLUME:

13)	$Vm = Vm(end) - Vm(begin)$	51.167 ft^3
14)	Y	0.9782
15)	$Vm' = Vm \cdot Y$	50.052 ft^3
16)	$Vpw @ t1 =$ from appendix	0.0000
17)	$corr\ Vwm = \{[(Vm' \cdot Vpw @ t1) / (Pm \cdot Tstd)] / (Tm \cdot Pstd)\}$	0.0000 ft^3
18)	$Vm\ std = \{[Vm' \cdot (Tstd/Tm) \cdot (Pm/Pstd)] - corr\ Vwm\}$	47.894 ft^3
19)	$Vlc = (\sum Volume\ of\ impingers)$	461.69 ml
20)	∂	0.002201 lb/ml
21)	R	21.85 Hg-ft^3/°R-lb-mo
22)	$MwH2O$	18.00 g/g-mo
23)	$Vw\ std = \{[(Vlc \cdot \partial \cdot R \cdot Tstd) / (Pstd \cdot MwH2O)] + corr\ Vwm\}$	21.7918 ft^3

CALCULATIONS:

MOISTURE-

24)	$Bws(1) = (Vw\ std) / (Vw\ std + Vm\ std) 100$	31.27 %
25)	$Vpw @ ts =$ from appendix	58.63 in Hg
26)	$Bws(2) = [(Vpw @ ts) / Ps] \cdot 100$	199.20 %
27)	$Bws =$ lower value of equation 24 or 26	31.27 %

MOLECULAR WEIGHT-

28)	$\%O2$	17.40 %
29)	$\%CO2$	3.20 %
30)	$\%N2 + inerts + \%CO$	79.40 %
31)	$Md = [0.440(\%CO2)] + [0.320(\%O2)] + [0.280(\%N2 + inerts + \%CO)]$	29.21 g/g*mole
32)	$Ms = Md \cdot (1 - Bws) + 18.0 \cdot (Bws)$	25.70 g/g*mole

FLOW-

33)	ΔP	0.445 in H2O
34)	Cp	0.846
35)	$vs = 85.49 \cdot Cp \cdot \{[(Ts \cdot \Delta P) / (Ps \cdot Ms)]^{.5}\}$	46.719 ft/s
36)	$As = 3.14 \cdot [(Ds)^2 / 4]$	9.51 ft^2
37)	$Qs = (vs) \cdot As \cdot 60$	2.66E+04 acfm
38)	$Qstd = 17.64 \cdot Qs \cdot (1 - Bws) \cdot Ps / Ts$	1.34E+04 dscfm

EMISSIONS-

FRONT HALF

39)	$mn\ (front)$	0.02492 g
40)	$Cs\ (front) = 15.43 \cdot mn(front) / Vm\ std$	0.0080 0.008 grains/dscf
41)	$E\ (front) = (0.00857) \cdot (Qstd) \cdot Cs\ (front)$	0.92 lbs/hr

BACK HALF

42)	$mn\ (back)$	0.08385 g
43)	$Cs(back) = 15.43 \cdot mn(back) / Vm = (12/\%CO2) \cdot Cs(back)$	0.0270 0.027 grains/dscf
44)	$E\ (back) = (0.00857) \cdot (Qstd) \cdot Cs\ (back)$	3.11 lbs/hr

TOTAL

45)	$mn\ (total) = mn(front) + mn(back)$	0.10877 g
46)	$Cs\ (total) = 15.43 \cdot mn(total) / Vm = (12/\%CO2) \cdot Cs(total)$	0.0350 0.035 grains/dscf
47)	$E\ (total) = (0.00857) \cdot (Qstd) \cdot Cs\ (total)$	4.03 lbs/hr

ISOKINETICS:

48)	$An = 3.14 \cdot [(Dn)^2 / 4]$	0.0755 in^2
49)	$I = .09450 \cdot (Ts \cdot Vm\ std) / Ps \cdot vs \cdot An \cdot (1 - Bws)$	107.88 % = 108 %

APPENDIX

SAN DIEGO AIR POLLUTION CONTROL DISTRICT, 9150 CHESAPEAKE DRIVE, SAN DIEGO, CA 92123

LABORATORY ANALYSIS OF PARTICULATE TEST

TEST SITE: Calmat-Pala
Pala Indian Reservation
Pala, CA 92059

TEST # 91301.0	P.O.# 117	TEST DATE: 10/28/91
LAB ANALYSIS BY: David N. Shina	<i>DN</i>	DATE: 11/6/91
LAB REPORT BY: David N. Shina	<i>DN</i>	DATE: 11/6/91
REVIEWED BY: Linda Twaddle		DATE:

(1) IMPINGER VOLUMES

	FINAL WEIGHT		INITIAL WEIGHT		NET WEIGHT
#1	807.96 g	-	552.38 g	=	255.58 g
#2	720.19 g	-	540.67 g	=	179.52 g
#3	469.17 g	-	458.16 g	=	11.01 g
#4	450.59 g	-	447.45 g	=	3.14 g
SILICA GEL CONTAINER:					
#5	828.87 g	-	816.43 g	=	12.44 g

Tot. Vol. = 461.69 g

(2) BLANKS

STD = Net Wgt(solv) / Tot. Vol(solv. used)

ACETONE:**VOLUMES:**

BKR ID = 91101
Initial = 200.00 ml
tot. Rinses = 30.00 ml
Tot. Vol = 230.00 ml

WEIGHTS:

final = 29.1812 g
initial = 29.1599 g
net = 0.0013 g

WATER:**VOLUMES:**

BKR ID = 91127
Initial = 200.00 ml
tot. Rinses = 30.00 ml
Tot. Vol = 230.00 ml

WEIGHTS:

final = 29.9974 g
initial = 29.9968 g
net = 0.0006 g

ORGANIC:**VOLUMES:**

BKR ID =
Initial = ml
tot. Rinses = ml
Tot. Vol = 0.00 ml

WEIGHTS:

final = g
initial = g
net = 0.0000 g

LIMIT: 0.001% = 10 ppm = 0.000010 g/ml

STD = 5.65217E-06 g/ml

0.000565 %

5.65 ppm

The Blank PASSED

LIMIT: 4ppm = 4mg/L = 0.000004 g/ml

STD = 2.60870E-06 g/ml

0.000261 %

2.61 ppm

The Blank PASSED

LIMIT: 0.001% = 10 ppm = 0.000010 g/ml

STD = N/A g/ml

N/A %

N/A ppm

The Blank N/A

(3) WEIGHT**FRONT HALF**

WEIGHT (uncorrected):

ACETONE
 BKR ID= 91114
 final= 29.1280 g
 initial= 29.1235 g

Wgt. Ac= 0.0045 g

VOLUME:

 Initial= 120.00 ml
 tot. rinses= 30.00 ml
 Sep funnel= 0.00 ml

Tot. Vol= 150.00 ml

WEIGHT FROM SOLVENT:

Total Vol * Acetone STD = 0.000848 g

WEIGHT (corrected):

Wgt(corr)= Wgt(unc)-Wgt from solvent= 0.003652 g

WEIGHT (uncorrected):

WATER:
 BKR ID= 91126
 final= 28.5938 g
 initial= 28.5716 g

Wgt. Water= 0.0220 g

VOLUMES:

 Initial= 250.00 ml
 tot. Rinses= 30.00 ml

Tot. Vol = 280.00 ml

WEIGHT FROM SOLVENT:

Total Vol * Water STD = 0.000730 g

WEIGHT (corrected):

Wgt(corr)= Wgt(unc)-Wgt from solvent= 0.021270 g

WEIGHT (uncorrected):

ORGANIC:
 BKR ID= _____
 final= _____ g
 initial= _____ g

Wgt. Org= 0.0000 g

VOLUMES:

tot. Rinses= _____ ml

Tot. Vol= 0.00 ml

WEIGHT FROM SOLVENT:

Total Vol * Organic STD = N/A g

WEIGHT (corrected):

Wgt(corr)= Wgt(unc)-Wgt from solvent= N/A g

WEIGHT:

FILTERS:
 ID No= _____
 final= _____ g
 initial= _____ g

Wgt. Filter= 0.0000 g

BACK HALF

WEIGHT (uncorrected):

ACETONE
 BKR ID= 91103
 final= 29.2957 g
 initial= 29.2921 g

Wgt. Ac= 0.0036 g

VOLUME:

 Initial= 150.00 ml
 tot. Rinses= 30.00 ml
 Sep. funnel= 0.00 ml

Tot. Vol= 180.00 ml

WEIGHT FROM SOLVENT:

Total Vol * Acetone STD = 0.001017 g

WEIGHT (corrected):

Wgt(corr)= Wgt(unc)-Wgt from solvent= 0.002583 g

WEIGHT (uncorrected):

WATER:
 BKR ID= 91061
 final= 49.5703 g
 initial= 49.4876 g

Wgt. Water= 0.0827 g

VOLUMES:

 Initial= 350.00 ml
 tot. Rinses= 40.00 ml
 Imp. charge= 197.53 ml

Tot. Vol= 587.53 ml

WEIGHT FROM SOLVENT:

Total Vol * Water STD = 0.001533 g

WEIGHT (corrected):

Wgt(corr)= Wgt(unc)-Wgt from solvent= 0.081167 g

WEIGHT (uncorrected):

ORGANIC:
 BKR ID= _____
 final= _____ g
 initial= _____ g

Wgt. Org= 0.0000 g

VOLUMES:

tot. Rinses= _____ ml

Tot. Vol= 0.00 ml

WEIGHT FROM SOLVENT:

Total Vol * Organic STD = N/A g

WEIGHT (corrected):

Wgt(corr)= Wgt(unc)-Wgt from solvent= N/A g

WEIGHT:

FILTERS:
 ID No= 89065
 final= 1.5966 g
 initial= 1.5965 g

Wgt. Filter= 0.0001 g

PARTICULATE COLLECTED (front half):

ΣWgt corrected + Wgt filter= mn (front)= 0.02492 g

PARTICULATE COLLECTED (back half):

ΣWgt corrected + Wgt filter= mn (back)= 0.08385 g

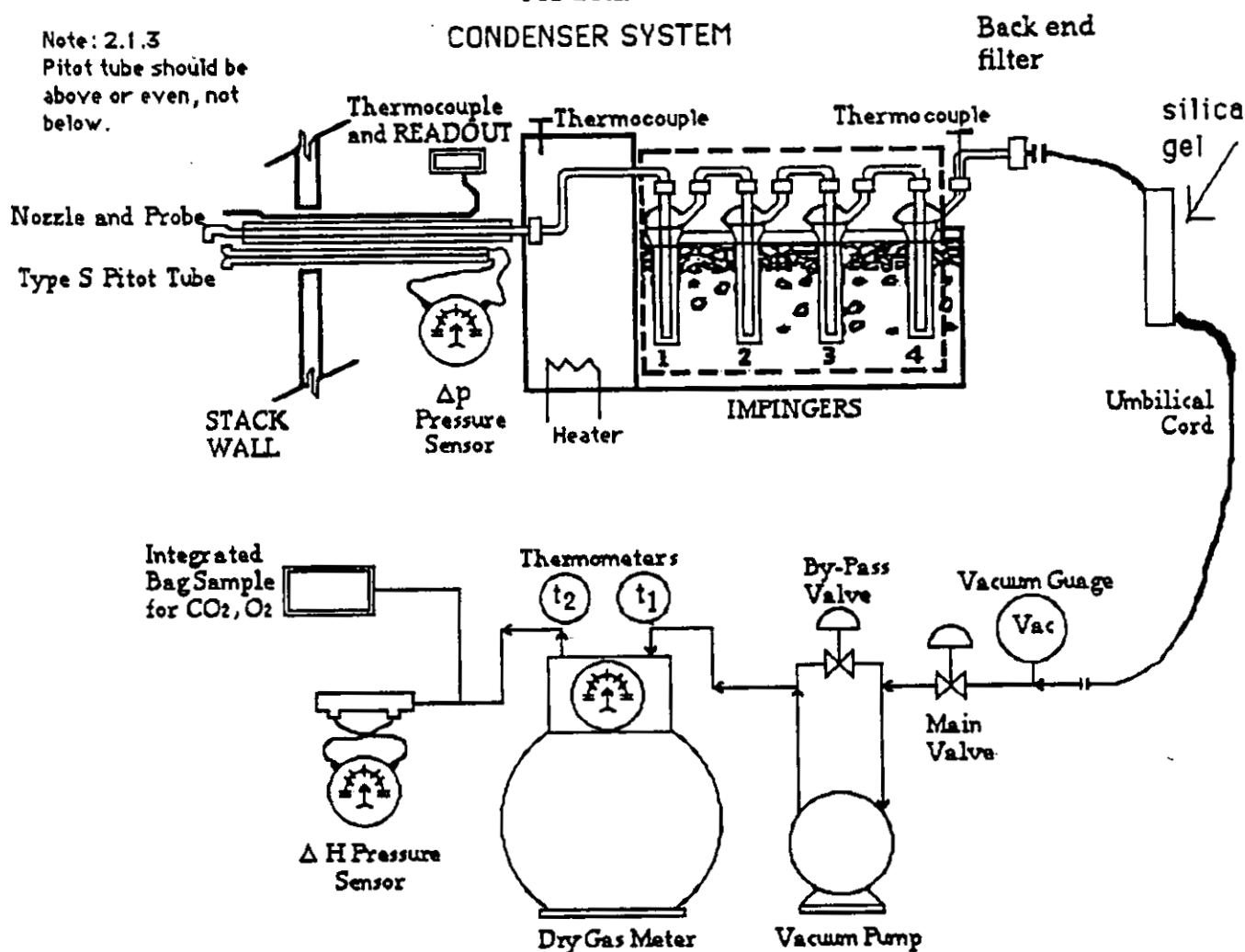
TOTAL PARTICULATE COLLECTED:

mn(front) + mn(back) = 0.10877 g

SAN DIEGO COUNTY AIR POLLUTION CONTROL DISTRICT

FIGURE 1

CONDENSER SYSTEM



LEGEND

No. 1 Mod- 100 ML Deionized Water
 No. 2 Std - 100 ML Deionized Water
 No. 3 Mod- Dry
 No. 4 Mod- Dry

 Mod - Modified Type Greenburg-Smith
 Std - Standard Type " "

FIELD DATA ABBREVIATIONS

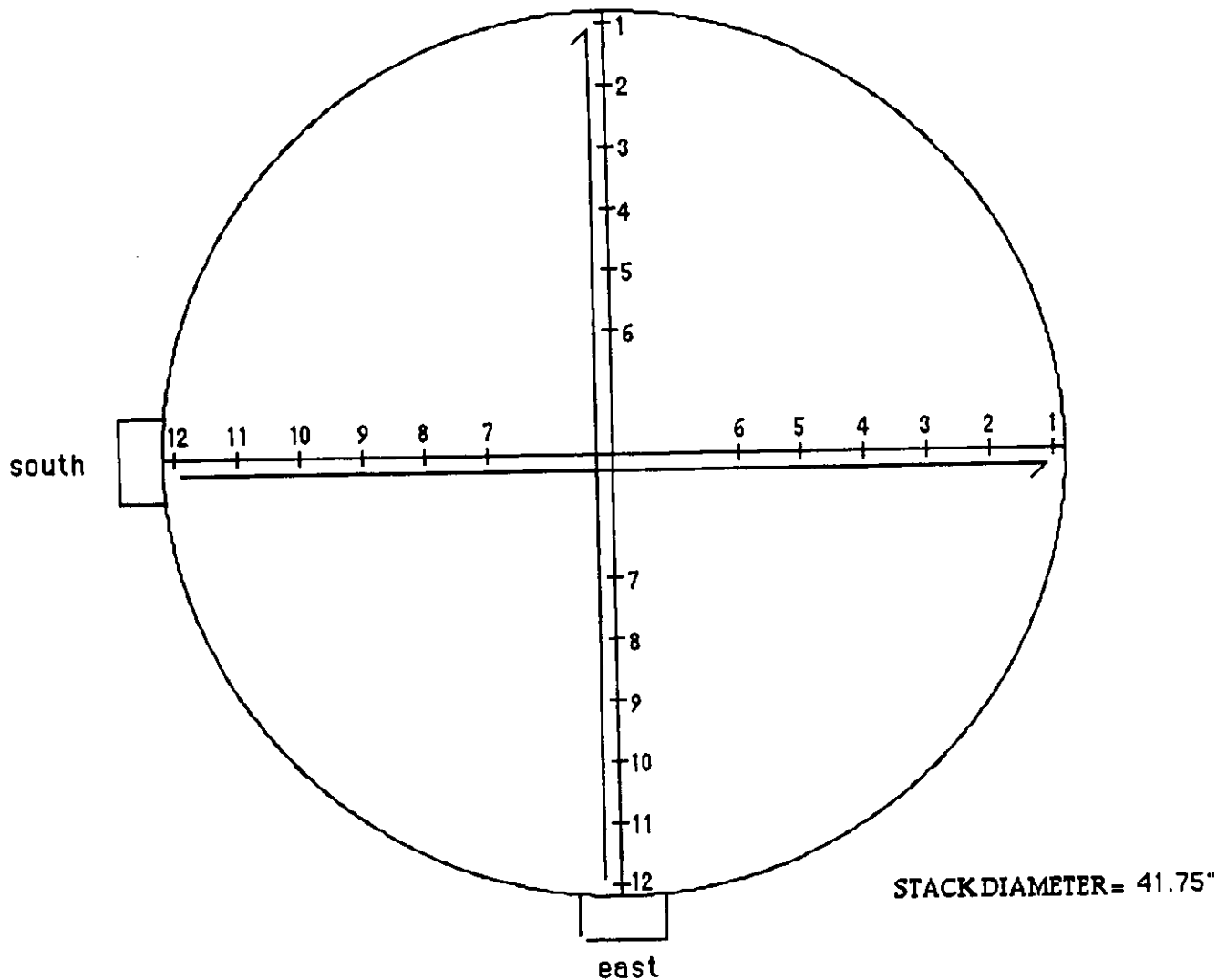
PT = Point Number
 T_s = Stack Temperature
 Δp = Pitot Tube Pressure Differential, in H₂O
 V_s = Stack Velocity, fps
 ΔH = Orifice Meter Pressure Drop, in H₂O
 t₁ = Meter Inlet Temperature, °F
 t₂ = Meter Outlet Temperature, °F
 P_m = Pump Vacuum, in Hg
 t_i = Impinger Temperature
 P_{bar} = Barometric Pressure

FIGURE 1 : PARTICULATE MATTER SAMPLING TRAIN

SAN DIEGO COUNTY AIR POLLUTION CONTROL DISTRICT

CALMAT-PALA

TRAVERSE POINTS



POINT	DISTANCE (inches)
1)	2.1
2)	6.7
3)	11.8
4)	17.7
5)	25.0
6)	35.6
7)	64.4
8)	75.0
9)	82.3
10)	88.2
11)	93.3
12)	97.9

FIGURE 2

Figure 3

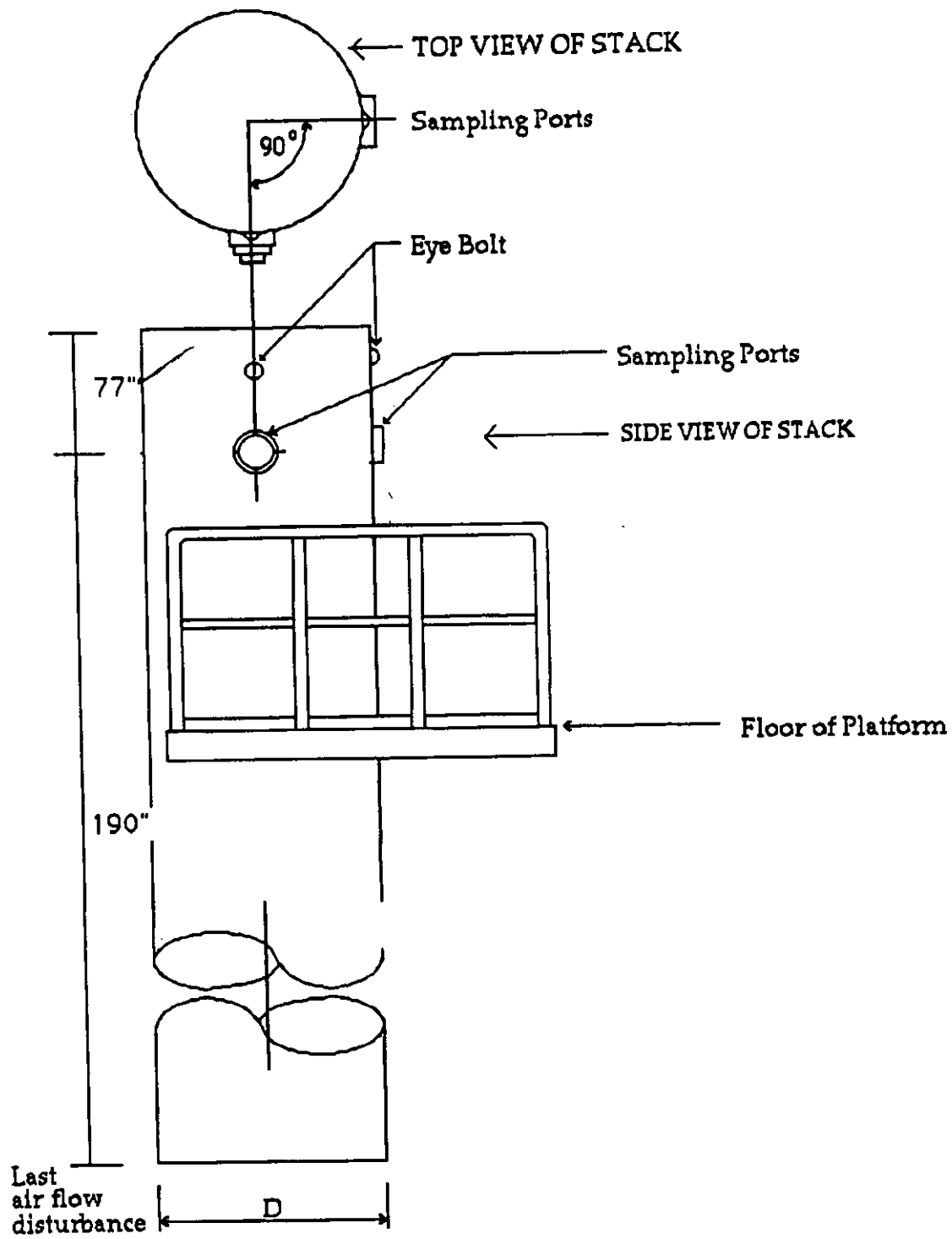


Figure 3

NOMENCLATURE

symbol	units	explanation	equation
A			
An	in ²	nozzle area	$\pi/4(D_n)^2$
As	ft ²	stack area	$\pi/4(D_s)^2$ or LxW
B			
Bws(1)	%	fractional stack gas moisture-equ 1	$((V_w \text{ std})/(V_w \text{ std}+V_m \text{ std}))100$
Bws(2)	%	fractional stack gas moisture-equ 2	$((V_{pw} @ t_s)/P_s)100$
Bws	%	water vapor in the gas stream	lower of Bws(1) and Bws(2)
C			
C12	gr/dscf	corr for grain loading at 12% CO2	$(12\%C_s)/(1\%CO_2)$
CO	%	carbon monoxide	read from measuring device (0 for Asphalt plants)
CO2	%	carbon dioxide	read from measuring device
Corr Vwm	ft ³	correction for Vw w/o silica gel	$((V_m * (V_{pw} @ t_s)/P_s) * P_m * T_{std}) / (T_m * P_{std})$
Cp	none	pilot tube correction factor	see EPA method 3
Cs(front)	gr/dscf	concentration of particulate in stack gas, corrected to STP-for front	$(15.43 * mn(\text{front})) / (V_m \text{ std})$
Cs(back)	gr/dscf	concentration of particulate in stack gas, corrected to STP-for back	$(15.43 * mn(\text{back})) / (V_m \text{ std})$
Cs(total)	gr/dscf	concentration of particulate in stack gas, corrected to STP-for total	$(15.43 * mn(\text{total})) / (V_m \text{ std})$
D			
∂ (density)	lb/ml	density of water at STP	0.002201 (see CRC)
Ds	in or ft	stack diameter	measure at site
Dn	in	nozzle diameter	avg of at least three measurements
E			
E.A.	%	Excess air (for combustion)	$((1\%O_2 - \%CO) * 100) / (26.1\%N_2 - \%O_2 - 5\%CO)$
E(front)	lbs/hr	part. emissions rate-front	$(0.00857)(Q_{sd} * C_s(\text{front}))$
E(back)	lbs/hr	part. emissions rate-back	$(0.00857)(Q_{sd} * C_s(\text{back}))$
E(total)	lbs/hr	part. emissions rate-total	$(0.00857)(Q_{sd} * C_s(\text{total}))$
H			
ΔH	in H2O	average differential pressure across the orifice meter	avg of the readings from the pressure measuring device
ΔH@	none	orifice pressure differential at STP	see EPA Method 5 Appendix
I			
I	%	isokinetics	$(0.09450 * T_s * V_m \text{ std}) / (P_s * v_s * \theta * (A_n / 144) * (1 - (Bws / 100)))$
M			
Md	g/g-mole	dry stack gas molecular wgt	$0.44(\%CO_2) + 0.320(\%O_2) + 0.280(\%N_2 + \text{inerts} + CO)$
mn(back)	g	particulate in impingers	measurement from lab analysis
mn(front)	g	particulate in nozzle & probe	measurement from lab analysis
mn(total)	g	total particulate collected	measurement from lab analysis
Ms	g/g-mole	wet stack gas molecular wgt	$Md(1 - Bws) + 18.0(Bws)$
MW CO2	g/mole	mo. wgt of carbon dioxide	44 (see periodic table)
MW N2	g/mole	mo. wgt of nitrogen	28 (see periodic table)
MW O2	g/mole	mo. wgt of oxygen	32 (see periodic table)
MW H2O	g/mole	mo. wgt of water	18 (see periodic table)
N			
N2	%	percent nitrogen	$100 - (\%CO_2 + \%O_2 + \%CO + \text{inerts})$
O			
O2	%	percent oxygen	read from measuring device

NOMENCLATURE (cont.)

NOMENCLATURE (concl.)

symbol	units	explanation	equation
P			
ΔP	in H ₂ O	pilot diff. press -velocity head of stack gas	read from measuring device
P_{bar} (p_i)	in Hg none	barometric pressure at sampling pt. the ratio of the circumference of a circle to its diameter	read from press measuring device 3.14165 (see CRC)
P_m	in Hg	absolute meter pressure	$P_{bar} + (\Delta H / 13.6)$
P_s	in Hg	absolute stack pressure	$P_{bar} + (P_{static} / 13.6)$
P_g	in H ₂ O	static pressure of stack	read from pressure sensing device
P_{std}	in Hg	press at std conditions (29.92)	see CFR
Q			
Q_s	acfm	flow rate	$vs \cdot A_o \cdot 60$
Q_{std}	dscfm	dry volumetric stack gas flow rate, corrected to STP	$17.64 \cdot Q_s (1 - Bws) \cdot (P_s / T_s)$
R			
R	in Hg-ft ³ /°R-lb-mo	ideal gas constant	21.85 (see CRC)
S			
S.L.	none	Sea Level	read from a relief map
T			
t_1	°F	dry gas meter inlet temp, uncorrected	read from temp sensing device
t_2	°F	dry gas meter outlet temp, uncorrected	read from temp sensing device
$t_1 \text{ corr}$	°F	dry gas meter inlet temp, corrected	$t_1 + \text{temperature correction}$
$t_2 \text{ corr}$	°F	dry gas meter outlet temp, corrected	$t_2 + \text{temperature correction}$
θ (theta)	min	sampling time / point	θ / t_m
θ (Theta)	min	total sampling time	none
t_i	°F	impinger outlet temp	read from temp sensing device
t_m	°F	dry gas meter temp in P	$(t_1 + t_2) / 2$
T_m	°R	dry gas meter temp in R	$t_m + 460$
t_n	none	tn number or traverse pts	summation of the traverse points
t_s	°F	stack temp in F	read from temp sensing device
T_s	°R	stack temp in R	$t_s + 460$
T_{std}	°R	temp at std conditions (528)	see CFR
U			
V_{lc}	ml	water collected from impingers and the silica gel (if applicable)	from lab analysis
V_m	ft ³	sample gas volume, uncorrected	read from dry gas meter
V_m'	ft ³	sample gas volume, corrected	$V_m \cdot Y$
$V_{m \text{ std}}$	ft ³	volume of gas sample by the dry gas meter, corrected to STP	$((V_m \cdot T_{std}) / P_m) / ((P_{std} \cdot T_m) - \text{corr } V_m)$
$V_{pw@ts}$	in Hg	vapor pressure of water at t_s	see CRC water vapor press. tables
$V_{pw@ti}$	in Hg	vapor pressure of water at t_i	see CRC water vapor press. tables
vs	ft/sec	stack gas velocity	$85.49 \cdot C_p (T_s \cdot \Delta P) / (P_s \cdot M_s)^{0.5}$
$V_{w \text{ std}}$	ft ³	Vol. of water vapor in gas sample, corrected to STP	$(V_{lc} \cdot \partial \cdot R \cdot T_{std}) / (P_{std} \cdot MW_{H_2O}) + \text{corr } V_{wm}$
V			
V	none	dry gas meter calibration factor	see CFR 40, parts 53-60

Conversion Factors

(multiply by the number)			
0.002669	in Hg-ft ³ /°R-ml	conversion to get in Hg-ft ³ /R	see CRC
0.00857	lb/gr-min/hr	conv from gr/min to lb/hr	see Lange's Handbook of Chemistry
0.04707	ft ³ /ml	conversion from ml to ft ³	see Lange's Handbook of Chemistry
15.43	gr/g	conversion from g to gr	see Lange's Handbook of Chemistry
85.49	(ft/sec)-(lb-in Hg/lb-mo-°R-in H ₂ O)) ^{0.5}	conversion factor to get velocity in ft/sec	see CRC
(divide by the number)			
144	in ² /ft ²	conversion from in ² to ft ²	see CRC
13.6	in H ₂ O/in Hg	conversion from in H ₂ O to in Hg	see CRC
(add to the number)			
460	°R/°F	conversion from F to R	see CRC

**Mechanical Engineering
Source Test Report
Permit Renewal Test**

Engineer: Earnest Davis
Test: Particulate Matter
P.O. no.: 0017
Test Start Time: 7:45

Test Date: 10/28/91
Source: Industrial Asphalt
Highway 76 Pala CA 92059
Test Stop Time: 8:15

Equipment Description: Hot-mix Asphalt Batch Plant

I Asphalt Production Data

<u>Bin #</u>	<u>MATERIAL NAME</u>	<u>TONS @ 8.33</u>	<u>TONS @ 8.59</u>	<u>Prod. Rate TPH</u>
AG1	Sand & Rock Dust	267.73	320.48	121.73
AG2	3/8" Rock	214.95	255.50	93.58
AG3	1/2" Rock	58.01	68.93	25.20
AG4	3/4" Rock	0.00	0.00	0.00
AG5	Filler	0.00	0.00	0.00
AC1	Asphalt Oil AR4000	62520	75168	29187
<u>AC2</u>	<u>Asphalt Oil AR8000</u>	<u>0.00</u>	<u>0.00</u>	<u>0.00</u>
Total		63060.69	75812.91	29427.51

II. Asphalt Composition for 1 Ton Batch

<u>Bin #</u>	<u>Material</u>	<u>3/8"</u>	<u>3/4"</u>	<u>Berm</u>	<u>1/2"</u>	<u>Sheet</u>
AG1	Sand & Dust	1146 lb.s	778 lb.s	1138 lb.s	908 lb.s	1816 lb.s
AG2	3/8" Rock	714	474	710	756	
AG3	1/2" Rock	0.00	380		209	
AG4	3/4" Rock	0.00	247			
AC5	Filler	20.00	19	20	19	20
AC1	Alt Oil AR4000	120.00	102		108	164
<u>AC2</u>	<u>Alt Oil AR8000</u>	<u>0.00</u>	<u>0.00</u>	<u>132</u>	<u>0.00</u>	<u>0 lbs</u>
Total		2000 lbs	2000 lbs	2000 lbs	2000 lbs	2000 lbs

III Summary of Data

Average production Rate : 240.50 TPH (excluding asphalt oil)

Material Temperature °F: $309 \pm 7^*$

Baghouse Pressure "H₂O: 4.8 ± 0.1

Exhaust Ammeter Amps : 75 ± 0

Fuel type: diesel

Fuel rate: 4.1 GPM

Burner Position (range): 80% to 85%*

Visible emissions (% opacity):

Baghouse exhaust stack : 0%

Rotary aft dryer seal : 0%**

Rotary forward dryer seal : 10% (generated intermittently)

Truck drop area : 20% ± 10 per drop ; blue smoke; less than 30 seconds duration per drop

Underground asphalt tank vent: 0% (no asphalt unloading was witnessed).

*During a 2 minute period of time proceeding an aggregate feed rate readjustment (slowing the throughput), the material temperature reached 327°F as the burner compensated with a corresponding minimum burner position of 29%.

**A gap existed between the burner assembly and the dryer drum ranging from 1 "at the top to 5" at the bottom (of the burner assembly/dryer drum interface). The flame of the burner was clearly visible.

RAW DATA SHEETS

Dashner

10/28/89

P.O. #117 (1/4)

dist. no. P.O. 015
Test # 91301

CPS

The $\Delta P_{avg} = .445$ in H_2O from test

<u>P_{slow}</u>	<u>Avg</u>	<u>C_{slow}</u>
.310	> .3083	.8427
.300		
.315		

<u>P_{middle}</u>		<u>C_{middle}</u>
.445	.445	χ

<u>P_{high}</u>		<u>C_{high}</u>
.670	> .7033	.8513
.760		
.680		

$$\frac{.445 - .3083}{.7033 - .3083} = \frac{\chi - .8427}{.8513 - .8427}$$

$$\frac{.1367}{.3950} = \frac{\chi - .8427}{.0086} ; .3461 = \frac{\chi - .8427}{.0086}$$

$$.0030 = \chi - .8427 ; \chi = .846$$

Dushin
10/28/91

P.O. #117

Culmnet-Pylo
Test # 91301 016

IMMUNOGENS (2/4)

PRE-TEST						POST-TEST			
date	Imp	WGT Imp	Imp + H ₂ O	WGT H ₂ O	Imp + H ₂ O + INSERT	date	WGT (all)	NBT GAN	COMMENTS
10/27	1	325.06	423.23	96.17	592.38	10/28	807.96	255.58	
	2	312.75	412.11	94.36	543.67		720.19	174.52	
	3	-	-	-	458.16		464.17	11.01	
	4	-	-	-	447.45		450.54	3.14	
	5	-	-	-	816.43		828.87	12.44	
Imp. Vol. = 19553 197.53 TOTAL =								461.69	

WEIGHTS

DATE	Beaker #	INIT WGT	WGT 1 11/4, 2pm	WGT 2 1p, 10am	WGT 3 11/6 9am	WGT 4	COMMENTS	FINAL
10/28	89065	1.5965	1.5968	1.5966	1.5966		white	1.5966
	91103	29.2921	29.2939	29.295	29.2957		clear	29.2957
	91061	49.4873	49.5702	5703	5703		black ppt	49.5703
	91114	29.1235	29.1282	1280	1280		some br. ppt	29.1280
	91126	28.5718	28.5939	5938	5938		tan ppt	28.5938
	91101	29.1599	29.1615	1613	1612		clear	29.1612
	91127	29.9968	29.9976	9974	9974		clear	29.9974

GAS

date	Trial 1 %, %	Trial 2 %	Trial 3 %	cal #	cal gas	Avg	COMMENTS	GAS
10/28	3.2	3.2	3.2	24.9	52	3.2		CO ₂
10/28	17.4	17.4	17.4	20.8	-	17.4		O ₂

SOLVENTS

Acetone: Omnisolve, EMSCIENCE
**H650AKO1160012, Lot # 9132

SUSLOW

10/28/91

P.O. #117

ACETOUS (3/4)

cc/mate-Pala 017
TEST # 91301

DATE	RINSE	VOL	Label	COMMENTS
10/28	INIT	120	Fr Ac	clear
10/29	10	30	91114	
	20			
TOTAL:				

DATE	RINSE	VOL	Label	COMMENTS
10/28	INIT	150	Back Ac	clear
	10	30	91103	
	20			
TOTAL:				

DATE	RINSE	VOL	Label	COMMENTS
10/28	INIT	200	Blank Ac	
	10	30	91101	
	20			
TOTAL:				

Dushkin
10/28/91

P.O. #117
WATER (H/A)

CC/MCH-Pg 19
018
TEST # 91301

DATE	RUN#	VOL	LABEL	COMMENTS
10/28	INIT	250	FR H ₂ O	
10/29	10	30	91126	Brown
	20			
TOTAL=				

DATE	RUN#	VOL	LABEL	COMMENTS
10/28	INIT	350	Back H ₂ O	
11	10	40	91061 91127	
	20			
TOTAL=				

DATE	RUN#	VOL	LABEL	
10/28	INIT	200	Blank water	
	10	30	91127	
	20			
TOTAL=				

BAROMETRIC PRESSURE REQUEST

SITE: Calmat - Pala TEST#: 91301 P.O.# 0117 DATE: 10/24/91

TO: HAZ ~~Tom Don~~ OF: Met DATE: 10/24

FROM: David S. OF: MTS DATE: 10/24

ADDRESS: Calmat Co. Highway 76 7mi E of I-15 Pala Indian Reservation

TEST DATE: 10/28/91

TEST TIME: 6am - 12pm

I need the usual hourly
breakdown

GRADE LEVEL: 550 Feet above MSL

+ - Feet above Grade

ALTITUDE: 550 Feet above MSL

CALCULATIONS:

06 - 29.43" Hg
07 - 29.44"
08 - 29.46"
09 - 29.46"
10 - 29.44"
11 - 29.42"
12 - 29.40"

7:30 - 9:00

$29.45 + 29.46 + 29.46 = 29.46$

SIGNATURE: [Signature]

DATE: 10/28/91

TIME: 1540 PST

METHOD 5 EQUIPMENT CHECKLIST

MISCELLANEOUS

- ☐ Camera & film
- ☐ Ice chest
- ☐ Ice
- ☐ 3 Tedlar bags
- ☐ Duct tape

TOOL BOX

- ☐ Assorted monkey wrenches
- ☐ Assorted open-end wrenches
- ☐ Assorted screwdrivers
- ☐ 3' pipe wrench
- ☐ Port (wire) brush
- ☐ Tape measure

SAFETY

- ☐ First aid box
- ☐ Hard hat
- ☐ Ear plugs
- ☐ Safety shoes
- ☐ Safety cones

LAB/FIELD EQUIPMENT

- ☐ Acetone
- ☐ Foil
- ☐ Parafilm
- ☐ Distilled water
- ☐ Kimwipes
- ☐ Vac. grease
- ☐ 100 ml graduated cylinder
- ☐ Sample collection bottles
- ☐ Nozzle brush
- ☐ Probe brush

CALCULATION EQUIPMENT

- ☐ Source Test brief case
- ☐ Calibration notebook
- ☐ Stopwatch
- ☐ Nomograph
- ☐ Calculator
- ☐ Assorted pens
- ☐ Tape measure
- ☐ White out (2 bottles)
- ☐ Labels
- ☐ Scissors
- ☐ Teflon tape
- ☐ L/S Box fuses

SAMPLING EQUIPMENT (main)

- ☐ L/S Box
- ☐ Pitot tube leak test equipment
- ☐ Thermocouple read-out
- ☐ Electrical cords (50' & 100')
- ☐ Umbilical cord
- ☐ Cold/Hot box
- ☐ Impingers (Impingers 1-4)
- ☐ Imp-imp connections
- ☐ Imp-probe connections
- ☐ Spare set of both sets of connections
- ☐ 100ml of water in 1st 2 impingers
- ☐ Impinger clips
- ☐ Silica gel impinger with vac. adapter
- ☐ Filter & Filter holder
- ☐ Spare filter & filter holder
- ☐ Heating coil
- ☐ Probe
- ☐ Spare probe
- ☐ Nozzle box (selection of nozzles & nuts)

SAMPLING EQUIPMENT (reserve)

- ☐ L/S Box
- ☐ Pitot tube leak test equipment
- ☐ Umbilical cord
- ☐ Cold/Hot box
- ☐ Impingers (Impingers 1-4)
- ☐ Imp-imp connections
- ☐ Imp-probe connections
- ☐ 100ml of water in 1st 2 impingers
- ☐ Impinger clips
- ☐ Silica gel impinger with vac. adapter
- ☐ Filter & Filter holder
- ☐ Heating coil

STACK EQUIPMENT

- ☐ Unirail
- ☐ Port/nipple adapters
- ☐ 2 C-clamps
- ☐ 2 unirails with rollers
- ☐ Chains
- ☐ 2 nylon straps
- ☐ Rope (25' and 50')
- ☐ Pail
- ☐ Gloves (leather)
- ☐ Gloves (heat resistant)
- ☐ Rags and diapers

EQUIPMENT DATA SHEET

SITE: Calmar Pal

TEST#: 91301

P.O.# 117

DATE: 10/28/91

EQUIPMENT CHECK:

MAIN:

	TYPE	ID#	SIZE	UNITS	CLEANED	CHECKED	CAL. DATE
Nozzle Dia.	Napp		1.310	in	DW	GDS	6/91
Pitot Tube	Napp	SU-7	5	ft	DW	GDS	6/91
Tedlar Bag	Sicc	calmar			DW	DW	—
L/S Box	Napp	0337	—	—	—	—	6/91
Stack Temp Sensor	Omega	N/A	—	—	—	—	6/91
Box Temp Sensor	Omega	N/A	—	—	—	—	6/91
Imp. Temp Sensor	Omega	N/A	—	—	—	—	6/91
ΔP Sensor	Dwyer	—	0-5	in H ₂ O	—	—	6/91
ΔH Sensor	Dwyer	—	0-5	in H ₂ O	—	—	6/91
Cold Box	Napp	Blue 4	—	—	—	—	—
Hot Box	Napp	Blue 4	—	—	—	—	—
Thermoc. Display	on L/S box	—	—	—	—	—	—

RESERVE

Nozzle Dia.							
Pitot Tube							
Tedlar Bag							
L/S Box							
Stack Temp Sensor							
Box Temp Sensor							
Imp. Temp Sensor							
ΔP Sensor							
ΔH Sensor							
Cold Box							
Hot Box							
Thermoc. Display							

SIGNATURE: DW

DATE: 10/27/91

TIME: _____

LAB DATA SHEET

SITE Calmat-Delta TEST#: P.O.#: 117 DATE: 10/28

COLD BOX#: Blue 4 HOT BOX#: Blue 4

PRE TEST MEASUREMENTS						POST-TEST		
	A	B	C	D	E		F	G
DATE	IMP No.	TRAP(w/o H2O) grams	TRAP (w/ H2O) grams	water (C-B) grams	INSERT H2O grams	DATE	MPINGER-H2O grams	H2O COLLECTED (F-E) grams
10/27	1	325.06 g	423.23 g	98.17 g	552.58 g	10/28	807.96 g	255.50 g
↓	2	312.75 g	412.11 g	99.36 g	540.67 g	↓	720.19 g	174.52 g
↓	3			— g	588.16 g	↓	466.17 g	11.01 g
↓	4			— g	447.45 g	↓	450.69 g	3.14 g
↓	5		816.113 g	— g	516.43 g	↓	828.87 g	12.44 g

197.53

TTL WGT GAIN FROM IMP (ΣG) 466.67 g

5N7

PreTest: SIGNATURE: 10/27/91 LEM C DATE: 12 pm TIME:
 PostTest: SIGNATURE: [Signature] DATE: 10/28 TIME: 1:30

GAS ANALYSIS

DATE	TRIAL	INSTRUMENT	RANGE	GAS	PERCENT
	1			CO2	3.2 %
	2			CO2	3.2 %
	3			CO2	3.2 %
	AVG			CO2	%
	1			O2	17.4 %
	2			O2	17.9 %
	3			O2	17.4 %
	AVG			O2	%

FILTER DATA

VARIABLE	WEIGHTS
(1) ID #	89065
(2) PRETEST	g
(3) POST-TEST	g
REC. AMT (3/2)	g

1.5907

cal # 24.9
51490 calgas CO2

PreTest: SIGNATURE: [Signature] DATE: 10/27 TIME: 12 pm
 PostTest: SIGNATURE: [Signature] DATE: 10/28 TIME: 1:30

Yc METER CHECK

SITE: Calmat - Pole TEST#: P.O#: #117 Date: 10/27

P bar= 29.41 in Hg L/S Box= 0337 $\Delta H@$ = 22254 T1 corr= +1.4 °F

Y= .4782 0.97*Y= .4489 1.03*Y= 1.0075 T2 corr= +1 °F

Yc=(5 min/Vm) * [((0.0319*Tm)/Pb)^0.5] run L/S box at $\Delta H@$ for 5 minutes

PRE-TEST 5 MINUTE Y CHECK

	Volume	t1 (unc)	t1 (corr)	t2 (unc)	t2 (corr)	(t1(c)+t2(c))/2
Initial(i)	496.892 ft ³	66 °F	66.4 °F	91.5 °F	91.6 °F	79 °F
final(f)	500.841 ft ³	68 °F	68.4 °F	107 °F	107.1 °F	87.75 °F

$V_m(f) - V_m(i)$
 Vm= 3.949 ft³

$(t_{avg-i} + t_{avg-f})/2$
 t_m = 83.38 °F T_m = 543.38 °R

Yc=(5 min/ 3.949 ft³) * [((0.0319 * 543.38 °R) / 29.41 in Hg)^{0.5}]= .4720

Vm Tm Pbar

0.97*Y < Yc < 1.03*Y = .4489 < .4720 < 1.0075 **PASS** FAIL

SIGNATURE: [Signature] DATE: 10/27 TIME: 12:50

POST-TEST 5 MINUTE Y CHECK

	Volume	t1 (unc)	t1 (corr)	t2 (unc)	t2 (corr)	(t1(c)+t2(c))/2
initial(i)	562.012 ft ³	74 °F	74.4 °F	102 °F	102.1 °F	88.25 °F
final(f)	565.863 ft ³	77 °F	77.4 °F	113.5 °F	113.6 °F	95.5 °F

$V_m(f) - V_m(i)$
 Vm= 3.851 ft³

$(t_{avg-i} + t_{avg-f})/2$
 t_m = 91.8 °F T_m = 551.88 °R

Yc=(5 min/ 3.851 ft³) * [((0.0319 * 551.88 °R) / 29.41 in Hg)^{0.5}]= 1.0045

Vm Tm Pbar

0.97*Y < Yc < 1.03*Y = .4489 < 1.0045 < 1.0075 **PASS** FAIL

[Signature]

10/28

2:15

Nomograph Calculations

TEST #:

Cellulose Pulp

DATE:

10/28

SITE

91301

P.O. #

117

Pm, absolute

29.53

Ps, absolute

29.43

Tm, absolute

85

ΔH@ across meter

2.7254

% moisture

20%

correction factor

1.150

Ts, absolute

245

ΔP stack

.2755 = .40

ideal nozzle diam

~~.264~~ .264

nozzle used

.310

test differential pressure

1.85 / .24 = 7.71

500

500

16887

72.0
24

3 min / pt

50
18451

59.10

24

2.4 min / pt

2.5 min / pt

Figure 5-8

SITE: _____

TEST#: _____

P.O. _____

DATE: _____

PIT	(AP end) in. H ₂ O	(AP start) in. H ₂ O	(AP calc = 0 to Pass), (15 sec. min.) in. H ₂ O	sec	P	F
PRE(-)	3.3	3.3	0	15	0	0
PRE(+)	2.7	2.7	0	15	0	0
POST(-)	3.1	3.1	0	15	0	0
POST(+)	2.1	2.1	0	15	0	0

VAC (Vend) - (Vstart) = (Vcalc = 0.02 cfm) @ (vac) in 1 min
ft³ ft³ ft³ in. Hg.

PRE: 55.584 - 50.584 - 0.01 @ 15 in 1 min (P) F

POST: 55.888 - 55.888 - 0.0 @ 9 in 1 min P F

OPER: _____

T1 corr: 4.4 °F T2 corr: 7.1 °F

Pbar _____ in Hg De: 3.48 in

Pa: -1.38 in H₂O T amb: UNK °F

Probe ID: _____ US box: 0.337

Probe len: 5 ft ΔH: 2.7254

Cp: _____ Y: 478.2

Dn: 1.310 in C. box: _____

K = 7.71 time/pt: 3.5 min

TRA PT NO	SAMPLING TIME min	GAS METER ft ³ , Vm Vm	PRESS DIFF ACROSS PIT TUBES in H ₂ O ΔP	PRESS DIFF. ACROSS THE ORIFICE in H ₂ O ΔH ΔH		STACK TEMP. °F °F	BOX TEMP. °F °F	IMPINGER TEMP. °F °F	DRY GAS TEMP °F		PUMP VAC in. Hg	CLOCK TIME Hr:min
				DESIRED	ACTUAL				INLET (T1)	OUTLET (T2)		
		506.861										7:45 start
1	2.5	508.041	.35	2.64	2.7	247		50	66	82	3	
2	5.0	509.885	.35	2.64	2.7	249	106	48	64	84	3	
3	7.5	511.975	.39	3.00	3.0	254	181	48	65	98	4	
4	10.0	514.123	.42	3.2	3.2	254		51	66	100	5	
5	12.5	516.443	.45	3.47	3.5	256	237	50	67	102	7	
6	15	518.802	.47	3.62	3.6	258	260	58	67	104	7	
7	17.5	521.325	.52	4.00	4.0	259	285		68	105	8	
8	20	523.682	.52	4	4	262	301	61	69	106	6.5	
9	22.5	525.932	.51	3.4	3.4	258	304	59	69.5	107	6	
10	25	528.232	.52	4	4	255	316	56	70	108	6	
11	27.5	530.458	.47	3.62	3.6	255	324	55	70	108	5.5	
12	30	532.630	.47	3.62	3.6	254	331	54	71	109	5.5	8:15 stop
1	2.5	534.569	.25	1.9	1.9	145	188	53	74	71	4	8:27 start
2	5.0	536.650	.37	2.85	2.4	140	226	48	74	102	5	
3	7.5	538.891	.42	3.2	3.2	242	246	47	73	106	5	
4	10.0	541.010	.43	3.46	3.5	259	278	46	73	108	5.5	
5	12.5	543.325	.50	3.85	3.9	260	299	47	74	110	6	
6	15	545.562	.50	3.85	3.4	261	311	47	74	110	6	
7	17.5	547.844	.51	3.4	3.4	260	316	48	74	111	6	
8	20	550.134	.51	3.4	3.4	258	308	48	75	112	6	
9	22.5	552.372	.48	3.7	3.7	258	310	48	75	113	6	
10	25	554.443	.43	3.3	3.3	257	322	50	76	114	5.5	
11	27.5	556.657	.46	3.5	3.5	256	332	50	77	114.5	6	
12	30	558.828	.43	3.3	3.3	253	340	51	78	116	5.5	8:46

??SITE NAME?? on ??TEST D.?? P.O.#????? TEST #?????
SAN DIEGO AIR POLLUTION CONTROL DISTRICT, 9150 CHESAPEAKE DRIVE, SAN DIEGO, CA. 92123

SOURCE TEST OF PARTICULATE EMISSIONS TO THE ATMOSPHERE

TEST SITE: Calmat Pala

TEST #: 91301

P.O.# 117

TEST DATE: 10/28/91

Type of plant (Asphalt / Perlite / Combustion):

asphalt

UNIT TESTED: Asphalt

EQUIPMENT: baghouse

TESTED BY: D. Shina et al

DATE: 10/28/91

SITE PERSONNEL: P. Mason

DATE: 10/28/91

APCD ENGINEER: E. Davis

DATE: 10/28/91

LAB ANALYSIS BY: D. Shina

DATE: 11/6/91

REPORT BY: D. Shina

DATE: 11/6/91

REVIEWED BY: L. Twaddle

DATE:

APPROVED BY:

DATE:

ROBERT YELENOSKY, SENIOR AIR POLLUTION CHEMIST

This report has been reviewed and found to be representative of the testing that was performed.

TEST	PERMIT LIMIT	MEASURED	PERFORMANCE
RULE 54 DUST & FUMES	40 lbs/hr	4.03 lbs/hr	PASSED

SUMMARY:

ITEM	Vm	Bws	Cs	E	I	Qstd	ts	PROD RATE
UNITS	ft ³	%	gr/dscf	lbs/hr	%	dscfm	°F	tons/hr
VALUE	51.167	31.27	0.035	4.033	108	1.34E+04	248	240.50

SYSTEM DESCRIPTION:

This asphalt plant combines crushed rock and sand with asphalt oil in batch loads of varying sizes. The rock and sand are heated in a rotary drum to dry them. The exhaust from this dryer is routed through a baghouse and finally to a stack. It is the emissions from this stack that are the subject of this report.

PROCEDURES:

The procedures and equipment utilized in these tests are based on EPA New Source Performance Standards Method 5. The sampling train was modified to utilize a back-end filter and 5th impinger filled with silica gel (fig. 1), as outlined by the SDAPCD QA manual.

CALCULATIONS

All preliminary assumptions and calculations are based on data obtained from previous tests. All equations are from EPA CFR 40, July 1, 1990, Parts 53-60, Appendix A, Methods 1-5 inclusive.

PARTICULATE SAMPLING:

The test consisted of sampling at 32 traverse points, 4 from each of 8 sample ports (fig.2), collected from 18 inches below the stack (fig.3). All field data was transferred to the computer printout. All calculations were done by the computer and the emissions were compared to rule 54 of the SDAPCD.

ANALYSES:

Gas: An integrated bag sample was collected during the test and analyzed at the APCD lab.

Particulate: All procedures follow EPA guidelines, except where noted in the SDAPCD QA manual.

EQUIPMENT:

All testing and analysis equipment was calibrated according to EPA guidelines.

Analysis:

Collection:

Sampling:

Temp./Press.:

CO2-Anarad AR400

Filter-Gelman

L/S Box-Napp

Thermocouples-Omega

O2-Teledyne Ryan 320 P4

Holder-Gelman

Umbilical cord-Napp

Read out-Omega

Macrobalance-Sargent Welch

Beakers-Pyrex

Cold/Hot box-Napp

Barometric-calc. by APCD

Microbalance-Sartorius

Impingers-Ace

Pitot tube-Napp

L/S box-Dwyer magnehelic

ver.4 APCD P/M-ISOS 9/10/91 by DNS

Printed: 11/20/91 @ 3:22 PM Page 1 of 3

??SITE.NAME?? on ??TEST DATE??

P.O.#????? TEST #?????

Trav. Pt	Vm (ft ³)	ΔP	ΔH	t 1(unc)	t 2(unc)	Stack Temp	Imp Temp	velocity
	508.861	(in H2O)	(in H2O)	(°F)	(°F)	(°F)	(°F)	(ft/sec)
1		0.350	2.700	68.00	82.00	247.00	50	41.36
2		0.350	2.700	64.00	84.00	249.00	48	41.42
3		0.390	3.000	65.50	88.00	254.00	48	43.88
4		0.420	3.200	66.00	100.00	254.00	51	45.54
5		0.450	3.500	67.00	102.00	256.00	56	47.20
6		0.470	3.600	67.00	104.00	258.00	58	48.31
7		0.520	4.000	68.00	106.00	259.00		50.85
8		0.520	4.000	69.00	106.00	260.00	61	50.88
9		0.510	3.900	69.50	107.00	259.00	59	50.32
10		0.520	4.000	70.00	108.00	255.00	56	50.70
11		0.470	3.600	70.00	108.00	255.00	55	48.20
12		0.470	3.600	71.00	109.00	254.00	54	48.17
1		0.250	1.800	74.00	71.00	149.00	53	32.45
2		0.370	2.900	74.00	102.00	190.00	48	40.78
3		0.420	3.200	73.00	108.00	242.00	47	46.15
4		0.450	3.500	73.00	108.00	259.00	46	47.30
5		0.500	3.900	74.00	110.00	260.00	47	49.89
6		0.500	3.900	74.00	110.00	261.00	47	49.93
7		0.510	3.900	74.00	111.00	260.00	48	50.39
8		0.510	3.900	75.00	112.00	258.00	48	50.32
9		0.480	3.700	75.50	113.00	258.00	46	48.82
10		0.430	3.300	76.00	114.00	257.00	50	46.17
11		0.460	3.600	77.00	114.50	256.00	50	47.72
12	558.028	0.430	3.300	78.00	116.00	253.00	51	46.04

Average:	Vm (ft ³)	ΔP (in H2O)	ΔH (in H2O)	t 1 (°F)	t 2 (°F)	ts (°F)	ti (°F)	vs (ft/sec)
	51.167	0.445	3.446	71.27	104.19	248	51	46.74

MISCELLANEOUS: Ø = 60.0 min tn = 24 points ø = 2.5 min	NOZZLE & PROBE: Dn = 0.310 in An = 0.0755 in ² Cp = 0.846	METER BOX PARAMETERS: ΔH _Q = 2.7254 Y = 0.9782 Box ID = D 337
PRESSURES: Pbar = 29.46 in Hg Pg = -0.38 in H2O Silica gel(yes/no) = YES Vpw @ ts = 58.63 in Hg Vpw @ ti = 0.0000 in Hg	VOLUME: start leak rate = 0.010 cfm Pass/Fail PASS final leak rate = 0.000 cfm Pass/Fail PASS Vm 51.167 ft ³	TEMPERATURES: t1 corr = 0.40 °F t2 corr = 0.10 °F tm = 88 °F ts = 248 °F ti = 51 °F
STACK PARAMETERS: circular (yes/no) = YES Ds = 3.48 ft Length = N/A ft As = 9.51 ft ²	LAB DATA: mn(front) = 0.02492 g mn(back) = 0.08385 g mn(total) = 0.10877 g Vlc 461.69 ml	STACK GAS MEASUREMENTS: CO2 = 3.20 % O2 = 17.40 % CO = 0.00 % N2 = 79.40 %

??SITE NAME?? on ??TEST DME??

TEMPERATURES:

- 01) $ts = (\sum ts(n))/total\ n's$
 02) $Ts = ts + 460$
 03) $tm = (\sum [(t_1(n) + t_2(n))/2])/total\ n's$
 04) $Tm = (t_1 + t_2)/2 + 460$
 05) $ti = (\sum ti(n))/total\ n's$
 06) $Tstd$

248 °F
 708 °R
 88 °F
 548 °R
 51 °F
 528 °R

PRESSURES:

- 07) $Pbar = ((P @ S.L.) + [ft. above S.L. * (-0.1 in Hg/100ft)])$
 08) $Pg = \text{read from pressure sensing device}$
 09) $Ps = Pbar + (Pg/13.6)$
 10) ΔH
 11) $Pm = Pbar + (\Delta H/13.6)$
 12) $Pstd$

29.46 in Hg
 -0.38 in H₂O
 29.43 in Hg
 3.44 in H₂O
 29.71 in Hg
 29.92 in Hg

VOLUME:

- 13) $Vm = Vm(end) - Vm(begin)$
 14) Y
 15) $Vm' = Vm * Y$
 16) $Vpw @ ti = \text{from appendix}$
 17) $corr\ Vwm = \{[(Vm' * Vpw @ imp/Ps) * Pm * Tstd]/(Tm * Pstd)\}$
 18) $Vm\ std = \{[Vm' * (Tstd/Tm) * (Pm/Pstd)] - corr\ Vwm\}$
 19) $Vlc = (\sum \text{Volume of impingers})$
 20) ∂
 21) R
 22) MwH_2O
 23) $Vw\ std = \{[(Vlc * \partial * R * Tstd)/(Pstd * MwH_2O)] + corr\ Vwm\}$

51.167 ft³
 0.9782
 50.052 ft³
 0.0000
 0.0008 ft³
 47.893 ft³
 461.69 ml
 0.002201 lb/ml
 21.85 Hg-ft³/°R-lb-mo
 18.00 g/g-mo
 21.7918 ft³

CALCULATIONS:**MOISTURE-**

- 24) $Bws(1) = (Vw\ std)/(Vw\ std + Vm\ std)100$
 25) $Vpw @ ts = \text{from appendix}$
 26) $Bws(2) = [(Vpw @ ts)/Ps] * 100$
 27) $Bws = \text{lower value of equation 24 or 26}$

31.27 %

58.63 in Hg

199.20 %

31.27 %

MOLECULAR WEIGHT-

- 28) %O₂
 29) %CO₂
 30) %N₂+inerts+%CO
 31) $Md = [0.440(\%CO_2)] + [0.320(\%O_2)] + [0.280(\%N_2 + \text{inerts} + \%CO)]$
 32) $Ms = Md * (1 - Bws) + 18.0 * Bws$

17.40 %
 3.20 %
 79.40 %
 29.21 g/g*mole
 25.70 g/g*mole

FLOW-

- 33) ΔP
 34) Cp
 35) $vs = 85.49 * Cp * \{[(Ts * \Delta P)/(Ps * Ms)]^{.5}\}$
 36) $As = 3.14 * [(Ds)^2/4]$
 37) $Qs = (vs) * As * 60$
 38) $Qstd = 17.64 * Qs * (1 - Bws) * Ps/Ts$

0.445 in H₂O
 0.846
 46.741 ft/s
 9.51 ft²
 2.67E+04 acfm
 1.34E+04 dscfm

EMISSIONS-**FRONT HALF**

- 39) $mn\ (front)$
 40) $Cs\ (front) = 15.43 * mn(front)/Vm\ std$
 41) $E\ (front) = (0.00857) * (Qstd) * Cs\ (front)$

0.0080

0.02492 g
 0.008 grains/dscf
 0.92 lbs/hr

BACK HALF

- 42) $mn\ (back)$
 43) $Cs\ (back) = 15.43 * mn(back)/Vm\ std$
 44) $E\ (back) = (0.00857) * (Qstd) * Cs\ (back)$

0.0270

0.08385 g
 0.027 grains/dscf
 3.11 lbs/hr

TOTAL

- 45) $mn\ (total) = mn(front) + mn(back)$
 46) $Cs\ (total) = 15.43 * mn(total)/Vm\ std$
 47) $E\ (total) = (0.00857) * (Qstd) * Cs\ (total)$

0.0350

0.10877 g
 0.035 grains/dscf
 4.03 lbs/hr

ISOKINETICS:

- 48) $An = 3.14 * [(Dn)^2/4]$
 49) $I = 0.09450 * (Ts * Vm\ std) / (Ps * vs * An * (1 - Bws))$

107.83 % =

0.0755 in²
 108 %

?? SITE NAME?? on ??TEST DATE??

P.O.#?????? TEST#??????

SAN DIEGO AIR POLLUTION CONTROL DISTRICT, 9150 CHESAPEAKE DRIVE, SAN DIEGO, CA 92123

LABORATORY ANALYSIS OF PARTICULATE TEST

TEST SITE: Calmat Pala

TEST # 91301.0	P.O.# 117	TEST DATE: 10/28/91
LAB ANALYSIS BY: D. Shina		DATE: 11/6/91
LAB REPORT BY: D. Shina		DATE: 11/6/91
REVIEWED BY: L. Twaddle		DATE: 11/20/91

(1) IMPINGER VOLUMES

FINAL WEIGHT	INITIAL WEIGHT	NET WEIGHT
#1 807.96 g	552.38 g	255.58 g
#2 720.19 g	540.67 g	179.52 g
#3 469.17 g	458.16 g	11.01 g
#4 450.59 g	447.45 g	3.14 g
SILICA GEL CONTAINER:		
#5 828.87 g	816.43 g	12.44 g
		Tot. Vol. = 461.69 g

(2) BLANKS

STD = Net Wgt(solv) / Tot. Vol(solv. used)

ACETONE:	WATER:	ORGANIC:
VOLUMES:	VOLUMES:	VOLUMES:
BKR ID = 91101	BKR ID = 91127	BKR ID =
Initial = 200.00 ml	Initial = 200.00 ml	Initial = ml
tot. Rinses = 30.00 ml	tot. Rinses = 30.00 ml	tot. Rinses = ml
Tot. Vol = 230.00 ml	Tot. Vol = 230.00 ml	Tot. Vol = 0.00 ml
WEIGHTS:	WEIGHTS:	WEIGHTS:
final = 29.1612 g	final = 29.9974 g	final = g
initial = 29.1599 g	initial = 29.9968 g	initial = g
net = 0.0013 g	net = 0.0006 g	net = 0.0000 g
LIMIT: 0.001% = 10 ppm = 0.000010g/ml	LIMIT: 4ppm = 4mg/L = 0.000004g/ml	LIMIT: 0.001% = 10 ppm = 0.000010g/ml
STD = 5.65217E-06 g/ml	STD = 2.60870E-06 g/ml	STD = N/A g/ml
0.000565 %	0.000261 %	N/A %
= 5.65 ppm	2.61 ppm	N/A ppm
The Blank PASSED	The Blank PASSED	The Blank N/A