

Note: This is a reference cited in *AP 42, Compilation of Air Pollutant Emission Factors, Volume I Stationary Point and Area Sources*. AP42 is located on the EPA web site at www.epa.gov/ttn/chief/ap42/

The file name refers to the reference number, the AP42 chapter and section. The file name "ref02_c01s02.pdf" would mean the reference is from AP42 chapter 1 section 2. The reference may be from a previous version of the section and no longer cited. The primary source should always be checked.

Firm
Permit Services
Enforcement
Technical Services
Source Inventory
Planning
Requester
DAPCO

BAY AREA
AIR QUALITY MANAGEMENT DISTRICT
939 Ellis Street
San Francisco, California 94109
(415) 771-6000

SUMMARY OF SOURCE TEST RESULTS

Report No. 91171

Test Date: 5/20/91

Test Times:

Run A: 0856-0946

Run B: 1018-1108

Run C: _____

SOURCE INFORMATION

BAAQMD REPRESENTATIVES

Firm Name and Address

KAISER SAND & GRAVEL
3311 Stanley Blvd.
Pleasanton, CA 94566

Firm Representative and Title

Mr. Larry Appleton,
Environmental Coordinator

Phone No. (415)846-8800

Source Test Engineers

C. McClure/H. Doi

Source:

S-11
Asphalt Plant

Permit Services Division / Enforcement Division

C. Berglund

Plant No.

103

Test Requested by:

J. Elliot (CDS)

Operates

on demand

Permit Conditions

None

Reg. Limit .04 gr/SDCF

Operating Parameters:

Plant operated continually during sampling producing 1600 tons of 1/2 inch aggregate asphalt. Dryer is natural gas fired consuming approximately 340 CFM at 350 TPH of production. Baghouse inlet averaged 320°F with a differential pressure of 2.8" H₂O. Moisture content of the aggregate averaged 4%.

Applicable Regulations: Regulation 10 Subpart I

VN Recommended: NO

Source Test Results and Comments:

METHOD: TEST

RUN A

RUN B

RUN C*

AVERAGE

LIMIT

ST-17	Stack Volume Flowrate, SDCFM				26,400	
	Stack Gas Temperature, °F	290	283		286	
ST-23	Water Content, Volume %	32.7	29.2		30.9	
ST-14	Oxygen, Volume %	10.6	11.6		11.1	
ST-5	Carbon Dioxide, Volume %	6.0	5.4		5.7	
ST-6	Carbon Monoxide, ppm	275	155		215	
	Carbon Monoxide lb/hr	31.5	17.8		24.6	
ST-15	Particulate, gr/SDCF	.013	.009		.011	.04
	Particulate, lb/hr	3.0	2.1		2.5	
	Isokinetic Ratio, Act/Theo	1.06	.92			

58" = 1.2/3.9/6.9/10.3/14.5/20.6/37.4/43.5/47.7/51.1/54.1/56.8/

* Run C not conducted due to failure of the probe heating system.

Note: P.E.R. conducted by C. Berglund, 0955-1029, Ringelmann 0.

$$MW = .44(5.7) + .32(11.1) + .28(53.2) + .18(30) = 26.36$$

430%
H₂O

CORRECTED COPY: This copy corrects errors in publishing results of Carbon Dioxide, Carbon Monoxide and Source Test Method Numbers.

NO COMMERCIAL USE OF THESE RESULTS IS AUTHORIZED

Source Test Team Leader

Date

C. McClure 6/5/91

Senior Source Test Engineer

Date

K. Kunaniec 6/11/91
K. Kunaniec

Approved by Source Test Manager

Date

G. Karels

6/12/91

DETAIL

ALAMEDA CO.

FOR CONTINUATION SEE MAP

35

442.

444.

432.

434.

36

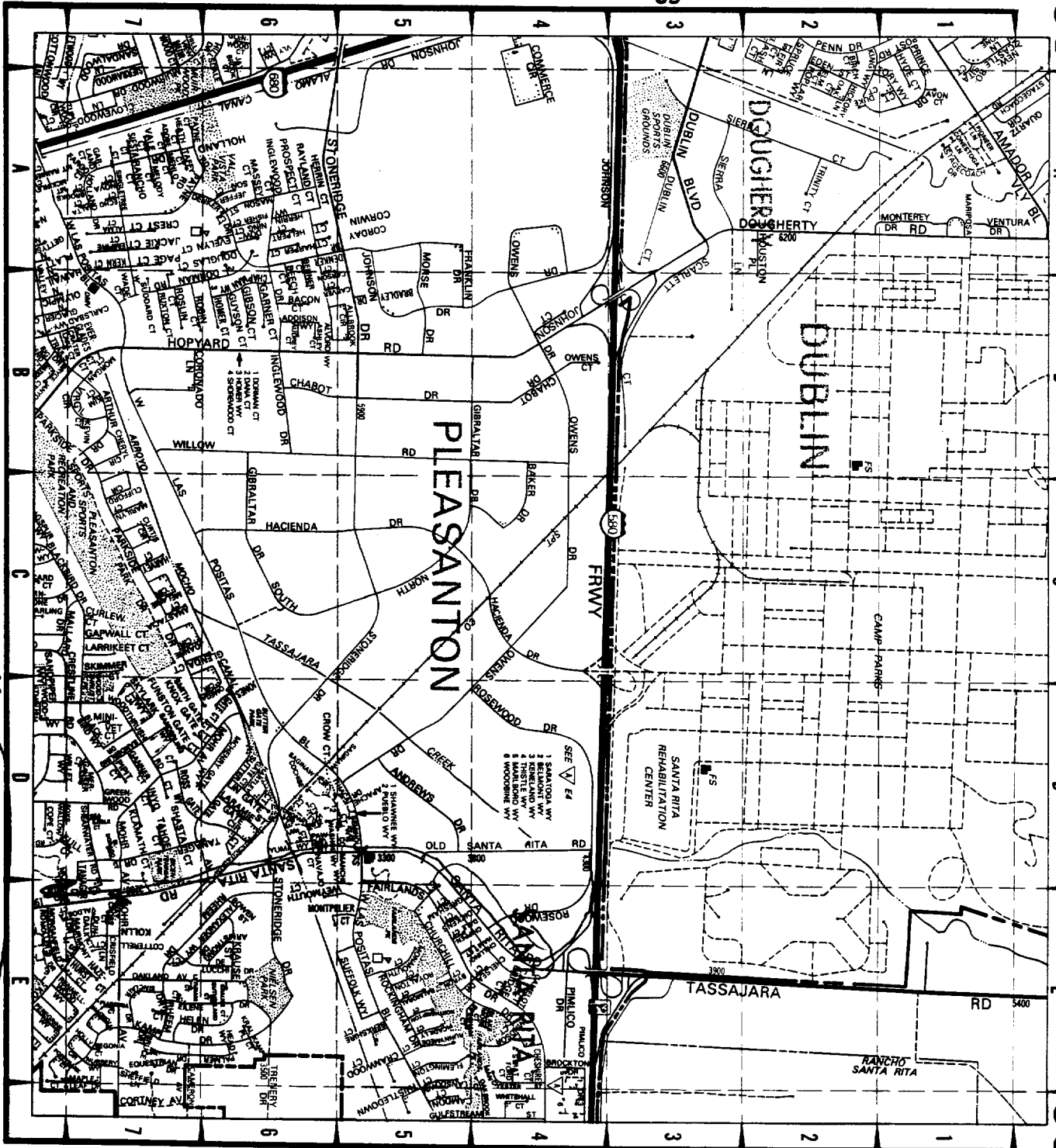
FOR CONTINUATION SEE MAP 34

36

FOR CONTINUATION SEE MAP

39

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1,590.

1,593.

FOR CONTINUATION SEE MAP 66

66

1,602.

1,605.

WALTER VIALI

FOR CONTINUATION SEE MAP

36

39

FOR CONTINUATION SEE MAP 37

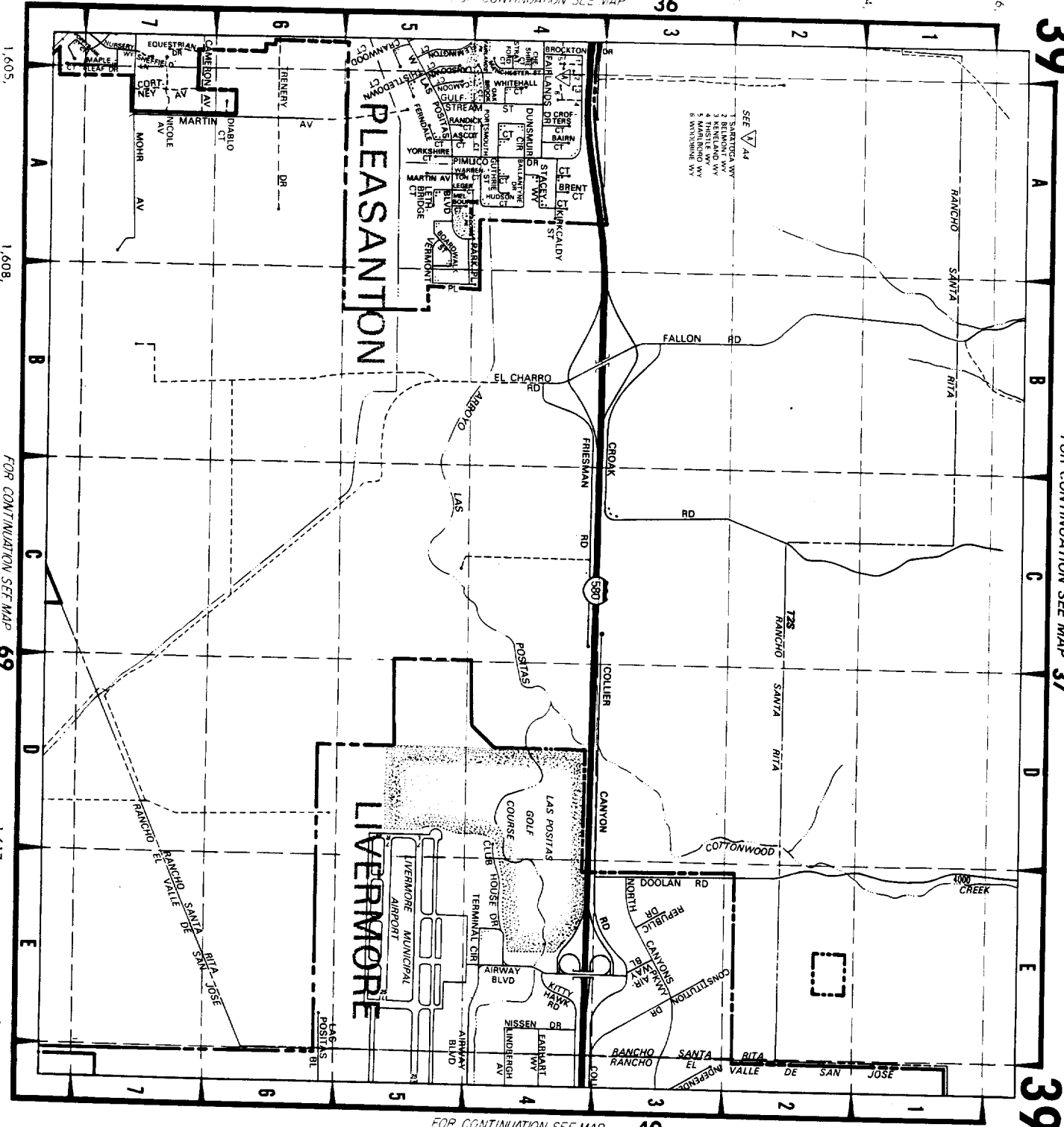
39

FOR CONTINUATION SEE MAP

40

DETAIL

ALAMEDA CO.



SOURCE TEST LAB DATA SHEET

PLANT: KAISER PLEASANTON

PAGE: 1 OF 1

SOURCE OPERATION: ASPHALT BAGHOUSE

INITIAL: KC

SOURCE TEST NO.:

TEST DATE: 07/14/92

FILTER MEDIA: GLASS FIBER, 110 MM

FILTER DATA

RUN #	FILTER #	TARE WEIGHT(g)		FINAL WEIGHT(g)		TOTAL(g)
A	637	.6113	.6115	.6279	.6278	.0163
B	638	.6085	.6087	.6286	.6286	.0199
C	639	.6078	.6080	.6168	.6170	.0088
DATE/TIME		4/7 AM	4/8 AM	7/20 AM	7/20 PM	

PROBE & NOZZLE RINSE DATA

RUN #	JAR #	TARE WEIGHT(g)		FINAL WEIGHT(g)		TOTAL(g)
A	1*	66.1446	66.1445	66.1589	66.1586	.0140
B	2	64.5983	64.5982	64.6060	64.6059	.0076
C	3	70.7015	70.7015	70.7086	70.7084	.0069
DATE/TIME		6/19 AM	7/9 PM	7/20 AM	7/20 PM	

TOTAL WEIGHTS (FILTER AND PROBE & NOZZLE)

RUN #	FILTER FINAL WT(g)	P & N FINAL WT(g)	TOTAL(g)
A	.0163	.0140	.0303
B	.0199	.0076	.0275
C	.0088	.0069	.0157

* 6/11 AM, 6/12 PM

SOURCE TEST LAB DATA SHEET

IMPINGER DATA

PLANT: KAISER, PLEASANTON

PAGE: 1 OF 1

SOURCE OPERATION: ASPHALT BAGHOUSE

INITIAL: KC/HD

SOURCE TEST NO.:

TEST DATE: 7/14/92

IMPINGER SOLUTION: DI H2O

DATA

IMPINGER#	A TARE WEIGHT(g)	B FILLED WEIGHT(g)	C FINAL WEIGHT(g)
P-1	497.5	597.5	747.0
P-2	483.2	583.2	586.4
P-3	491.4	591.4	740.6
P-4	495.1	595.1	615.5
P-5	467.4	567.4	737.2
P-6	489.2	589.2	594.1

IMPINGER#	C-A SAMPLE WEIGHT(g)	C-B CONDENSATE WT(g)	TOTAL WEIGHT(g)
P-1	249.5	149.5	RUN A
P-2	103.2	3.2	152.7
P-3	249.2	149.2	RUN B
P-4	120.4	20.4	169.6
P-5	269.8	169.8	RUN C
P-6	104.9	4.9	174.7

GRAIN LOADING $G_{gr}/SCF = 15.43 \cdot \frac{W_p(g)}{V_o(SCF)}$

KANSER #103
S-11 PLEASANTON
7/14/92

$$G_A = 15.43 \frac{(0.0303)}{20.809} = \underline{0.022 gr/SCF}$$

$$W_{PA} = 0.0303g$$

$$G_B = 15.43 \frac{(0.0275)}{21.77} = \underline{0.019 gr/SCF}$$

$$W_{PB} = 0.0275g$$

$$G_C = 15.43 \frac{(0.0157)}{23.032} = \underline{0.010 gr/SCF}$$

$$W_{PC} = 0.0157g$$

$$G_{AVG} = \underline{0.017 gr/SCF}$$

$$V_{OA} = 20.809 SCF$$

$$V_{OB} = 21.77 SCF$$

$$V_{OC} = 23.032 SCF$$

MASS EMISSIONS $M = \frac{G \cdot Q_o}{116.67}$

$$M_A = (0.022) \frac{(2512P)}{116.67} = \underline{4.7 Lb/HR}$$

$$Q_o = 2512 SCFM$$

$$M_B = \underline{4.1 Lb/HR}$$

$$M_C = \underline{2.1 Lb/HR}$$

$$M_{AVG} = \underline{3.6 Lb/HR}$$

ISOKINETIC RATIOS

E.P.A. EQUATION

5-8

$$R_I = \frac{(T_s \text{ } ^\circ\text{R})(V_o \text{ SDCF})(K_I)}{(V_s \text{ FPS})(100 - \% \text{H}_2\text{O})(A_n \text{ FT}^2)(t \text{ MINUTES})(P_s \text{ "Hg})}$$

$K_I = 9.414 \times 10^{-2}$
AT STANDARD
CONDITIONS OF
29.92" Hg & 70°F

$$P_s = P_{\text{BAR}} + \left(\frac{P_{\text{STATIC}} \text{ "H}_2\text{O}}{13.6 \text{ "H}_2\text{O/"Hg}} \right) = 29.98 + \left(\frac{-0.25}{13.6} \right)$$

$$P_s = 29.962 \text{ "Hg} \quad t = \text{TIME} = 50 \text{ MINUTES}$$

$$A_n = 8.454 \times 10^{-4} (D_n \text{ cm})^2 \text{ FT}^2$$

$$D_n = 6.2 \text{ mm} = .62 \text{ cm}$$

$$A_n = 8.454 \times 10^{-4} (.62 \text{ cm})^2 \text{ FT}^2$$

$$A_n = 3.25 \times 10^{-4} \text{ FT}^2$$

GROUP TERMS:

$$R_I = \frac{(T_s)(V_o)(9.414 \times 10^{-2})}{(V_s)(100 - \% \text{H}_2\text{O})(3.25 \times 10^{-4})(50)(29.962)} = \frac{(T_s)(V_o)(.19337)}{V_s(100 - \% \text{H}_2\text{O})}$$

$$\text{RUN A) } T_s = 681.4 \text{ } ^\circ\text{R} \quad V_o = 20.809 \text{ SDCF} \quad V_s = 40.48 \text{ FPS} \quad \% \text{H}_2\text{O} = 26.1 \quad 100 - \% \text{H}_2\text{O} = 73.9$$

$$R_{IA} = \frac{(681.4)(20.809)(.19337)}{(40.48)(73.9)} = 0.916 = \underline{\underline{0.92}}$$

$$\text{RUN B) } T_s = 688 \text{ } ^\circ\text{F} \quad V_o = 21.77 \text{ SDCF} \quad V_s = 41.01 \text{ FPS} \quad \% \text{H}_2\text{O} = 27.1 \quad 100 - \% \text{H}_2\text{O} = 72.9$$

$$R_{IB} = \frac{(688)(21.77)(.19337)}{(41.01)(72.9)} = 0.968 = \underline{\underline{0.97}}$$

$$\text{RUN C) } T_s = 681 \text{ } ^\circ\text{F} \quad V_o = 23.032 \quad V_s = 42.89 \text{ FPS} \quad \% \text{H}_2\text{O} = 26.7 \quad 100 - \% \text{H}_2\text{O} = 73.3$$

$$R_{IC} = \frac{(681)(23.032)(.19337)}{(42.89)(73.3)} = 0.965 = \underline{\underline{0.96}}$$

#103
PLANT: KAISER% PLEASANTON
SOURCE: S-11
DATE: 7/14/92

GAS ANALYSIS

SPAN CYLINDER # LL10543

KAISER S&G #103

5-11

7/14/92

GAS	SPAN VALUE	SPAN UNITS
O ₂	20.95%	7.65u
CO ₂	14.8%	6.53u
CO	1210PPM	5.45u

RUNA)

O ₂	CO ₂	CO
5.48	1.84	.15
5.05	2.00	.15 < L.O.D.
5.12	2.03	.20
5.10	1.94	.20
<u>5.15</u>	<u>1.95</u>	<u>.18</u>
$\bar{x} = 5.18u$	$\bar{x} = 1.95u$	

$$\frac{20.95\%}{7.65u} \times \frac{X\%O_2}{5.18u}$$

$$\frac{14.8\%}{6.53u} \times \frac{X\%CO_2}{1.95u}$$

< LOD_{CO}

$$\frac{20.95\%}{7.65u} \times \frac{X\%O_2}{5.02u}$$

$$\frac{14.8\%}{6.53u} \times \frac{X\%CO_2}{2.02u}$$

$$\frac{1210PPM}{5.45u} \times \frac{XPPMCO}{0.176u}$$

$$\frac{20.95\%}{7.65u} \times \frac{X\%O_2}{5.41u}$$

$$\frac{14.8\%}{6.53u} \times \frac{X\%CO_2}{1.84u}$$

$$\frac{1210PPM}{5.45u} \times \frac{XPPMCO}{0.212u}$$

RUNB)

O ₂	CO ₂	CO
4.67	2.28	.15
5.07	1.87	.15
5.14	2.04	.20
<u>5.19</u>	<u>2.01</u>	<u>.20</u>
$\bar{x} = 5.02u$	$\bar{x} = 2.02u$	$\bar{x} = 0.176u$

RUNA
O₂ = 14.2%

CO₂ = 4.4%

CO = < L.O.D.

RUNB
O₂ = 13.7%

CO₂ = 4.6%

CO = 40PPM

RUNC
O₂ = 14.8%

CO₂ = 4.2%

CO = 50PPM

RUNC)

O ₂	CO ₂	CO
5.60	1.84	.25
5.44	1.73	.20
5.60	1.68	.20
<u>5.00</u>	<u>2.10</u>	<u>.20</u>
$\bar{x} = 5.41u$	$\bar{x} = 1.84u$	$\bar{x} = 0.212u$

O_{2AVG} = 14.2%

CO_{2AVG} = 4.4%

CO_{AVG} ≈ 40PPM

DISTRIBUTION:

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BAY AREA
AIR QUALITY MANAGEMENT DISTRICT
939 Ellis Street
San Francisco, California 94109
(415) 771-6000

SUMMARY OF SOURCE TEST RESULTS

Report No. 93003Test Date: 07/14/92

Test Times:

Run A: 0747-0837Run B: 0857-0947Run C: 1000-1050

SOURCE INFORMATION

BAAQMD REPRESENTATIVES

Firm Name and Address

KAISER SAND & GRAVEL
3311 Stanley Blvd.
Pleasanton, CA 94566

Firm Representative and Title

Mr. Larry Appleton,
Environmental Coordinator

Phone No. (510) 846-8800

Source: S-11 Asphalt Plant

Plant No. 103

Operates on demand

Source Test Engineers

C. McClure/H. Doi

Observers:

A. Tikku, R. Hammervold

Permit Services Division / Enforcement Division

M. Wagner

Test Requested by:

J. Elliot (CDS) (NSPS)

Permit Conditions

None

Operating Parameters:

Plant operated continually at a rate of 325 ton per hour producing 1600 ton of 3/4" Aggregate Asphalt during sampling. Rotary Kiln is Natural Gas fired consuming an average of 221 C.F.M.. Baghouse inlet temperature varied between 220-250°F with a differential pressure of 1.4 inches w.c..

Applicable Regulations:

Regulation 10, Subpart I

VN Recommended: NO

Source Test Results and Comments:

METHOD:	TEST	RUN A	RUN B	RUN C	AVERAGE	LIMIT
ST-17	Stack Volume Flowrate, SDCFM				25,100	
	Stack Gas Temperature, °F	222	228	222	224	
ST-23	Water Content, Volume %	26.1	27.1	26.7	26.6	
ST-14	Oxygen, Volume %	14.2	13.7	14.8	14.2	
ST-5	Carbon Dioxide, Volume %	4.4	4.6	4.2	4.4	
ST-6	Carbon Monoxide, ppm	* <20	40	50		
	Carbon Monoxide, lb/hr	<2.2	4.4	5.5		
ST-15	Particulate, gr/SDCF	.022	.019	.010	.017	.04
	Particulate, lb/hr	4.7	4.1	2.1	3.6	
	Isokinetic Ratio, Act./Theo.	.92	.97	.96		

* A "<" indicates results less than instrument limit of detection.

NOTE: P.E. R. 0930-0944 by R. Pilkington, Ringelmann O to 1/2. See attached report.

NO COMMERCIAL USE OF THESE RESULTS IS AUTHORIZED

Air Quality Engineer II

Date

C. McClure # 7/24/92
C. McClure

Supervising Air Quality Engineer

Date

K. Kunaniec 7/27/92
K. Kunaniec

Approved by Source Test Manager

Date

G. Karels
G. Karels

7/27/92



BAY AREA AIR QUALITY MANAGEMENT DISTRICT
939 Ellis Street, San Francisco, Calif. 94109 • 771-6000

Source Test Data Sheet

6.2mm Nozzle Diameter
I-60 P-66 .813 Pilot Tube
VAN#12 Gas Collector No.
29.98 Barometric Pressure
0.00222 Leak Rate
5 TIME EACH POINT
10 # OF POINTS
50 TIME EACH RUN

Source Operation S-11
H/O3 LAGER ALKALINITY
PARTICULATE COMBUSTION
B/H STACK
R-58"
-2.5% H₂O
25-30%
ASSUMED H₂O

Source Test No. TBA
Run No. 7/14/92
Date:

MAG GAGE RACK #112-111 METER(X)=0.98214

METER# 510950 → EXH.

SAMPLING										REMARKS			
Traverse Point	Dist. From 1.222L inches	INITIAL TRAVERSE		Traverse Point	AP H ₂ O	V _g PPS	Time	METER			Vac "Hg	Sat'd Gas Temp OF	T _g Duct Temp OF
		Duct Temp OF	ΔP H ₂ O					Rate CFH	Temp OF				
15 = 242													
1 .09	1.2	B-1	.20	4-3	.12	22.2	5	14.1	70	74.61	3	37	210
2 .11	3.9	2	.25	4	.10	20.3	10	12.8	70	75.69	3	40	215
3 .13	6.9	3	.32	5	.13	23.2	15	14.6	70	76.99	3	40	216
4 .13	10.3	4	.40	6	.18	27.3	20	17.2	70	78.37	3	40	217
5 .14	14.5	5	.40	7	.44	42.8	25	26.7	71	80.65	5	41	222
6 .17	20.6	6	.47	8	.60	50.7	30	30.8	72	83.23	9	41	242
7 .44	37.4	7	.50	9	.65	52.1	35	32.4	73	85.92	10	42	225
8 .52	43.5	8	.42	10	.70	54.1	40	33.7	73	88.74	10.5	43	224
9 .70	47.7	9	.42	11	.80	57.8	45	36.0	74	91.75	13	44	223
10 .80	51.1	10	.50	12	.72	54.8	50	34.2	74	94.63	11.5	42	223
11 .85	54.1	11	.50				(6837)		(71.7)	21.19	(7.1)	(41.0)	(221.7)
12 .80	56.8	12	.50						(531)	X. 98214			(681.4)

OVER THE TOP

Source Test Team
CHUCK McCLURE
Source Test Engineer II
H. 100E

Condensate 156 (g)
V₀ 20.00
1120 36.2
-200
156

3.04

$$Q_m = \left[\frac{V_s (100 - \text{H}_2\text{O})}{75.70} \right] \left[\frac{V_s}{T_s} \right]$$

$$V_s = (K)(CP) \left[\frac{T_s \cdot \Delta P}{(P_b - P_s) \cdot (P_b - P_s)} \right] \left[\frac{P_b}{P_s} \right]$$

$$V_0 = 17.71 (V_m)(P_b) \left[\frac{T_m}{T_s} \right]$$

B/H



BAY AREA AIR QUALITY MANAGEMENT DISTRICT
939 Ellis Street, San Francisco, Calif. 94109 • 771-6000

Source Test Data Sheet

01-01

Source Operation 17,000 S-11 76.92 MIN 221 CFM

Plant

Sample Type #103

Process Cycle PARTICULATE & COMBUSTION

Duct Size 8" H SINK

Duct Pressure 12-58"

Assumed H_2O 2.25% H_2O

Source Test No. B

Run No. 7115/192

Date: 7/15/92

6.2 mm Nozzle Diameter

813 Pitot Tube

VAN#12 Gas Collector No.

29.98 Barometric Pressure

0.003089 Leak Rate

5 TIME EACH POINT

10 # OF POINTS

50 TIME EACH RUN

MAG GAGE RACK # V12-11 METER (X) = 98214

METER # 510950 → EXH.

Sampling Train: PROBE → FILTER # 638 → IMP # 1-5 IMP # 1-5															
Traverse Point	Dist. From inches	INITIAL TRAVERSE		SAMPLING										REMARKS	
		Duct Temp of	ΔP H ₂ O	Traverse Point	ΔP H ₂ O	V _s FPS	Time 08570	Rate CFH	METER Temp of	Volume Ft ³	Vac "Hg	Sat'd Gas Temp of	T _s Duct Temp of		
				B-3		.27	32.7	5	22.8	76	96.77	5	34	190	
				4		.22	30.5	10	19.9	77	98.47	5	37	232	
				5		.30	35.7	15	23.2	77	100.41	5.5	38	237	
				6		.42	42.3	20	27.4	77	102.68	7	38	239	
				7		.38	40.1	25	26.2	78	104.90	8	39	234	
				8		.43	42.8	30	27.7	78	107.23	8	39	239	
				9		.47	44.5	35	29.2	79	109.66	9	40	229	
				10		.55	48.1	40	31.6	79	112.23	11	40	228	
				11		.52	46.7	45	30.8	79	114.79	10.5	39	226	
				12		.50	45.7	50	30.2	80	117.33	10	41	225	
										78.0	22.46	7.9	38.5	227.9	
										538	X.98214			688	
														22.059	

Source Test Team
DUCK MCCLURE
Source Test Engineer II

A. TIKKUL

R. HAMMERVOLD

PERMITS
B. WUNDER

Condensate 170 (g)

802.08 V₀ 217.54 F

1120 27.0

120

250

370

- 170

$$D_n = 13.7 \left[\frac{T_s + 460}{V_s (100 - RH_2O)} \right]^{1/2}$$

$$Q_m = \left[(2.638 \times 10^{-3}) \frac{(100 - RH_2O)^{1/2}}{T_s} \right] V_s \times 540$$

$$V_s = (K)(C_p) \left[\frac{T_s \cdot \Delta P}{V_m (P_b)} \right] \frac{8549}{T_m \cdot 538}$$

$$V_0 = \frac{17.71 (V_m)(P_b)}{T_m \cdot 538}$$



Source Test Data Sheet

BAY AREA AIR QUALITY MANAGEMENT DISTRICT
939 Ellis Street. San Francisco, Calif. 94109 • 771-6000

6.2mm Nozzle Diameter
0.2 Pitot Tube

Source Operation	5-11 ASABART
Plant	#103 LEASED ALUMINUM
Sample Type	BASIC OXIDE GAS
Process Cycle	B/H STACK
Duct Size	2-58"
Duct Pressure	-2.5" H ₂ O
ASSUMED H ₂ O	27%

Source Test No.

Run No.

Male:

VAN #12065 CORRECT
 29.98 Barometric Pressure
 2.503223 Leak Rate
 TIME EACH RUN
 # OF POINTS
 5
 10
 50
 TIME EACH RUN

max. rate = 80-1 #1/2-11 METER (Y) = 98214

EXH. 7080-1

SAMPLING														
Traverse Point	Dist. From inches	INITIAL TRAVERSE		Traverse Point	ΔP H ₂ O	Vg FPS	Time	Rate CFH	METER		Vac "Hg	Sat'd Gas Temp OF	T _g Duct Temp OF	REMARKS
		Duct Temp OF	ΔP						Temp OF	Volume Ft ³				
B-3					30	34.9	1000	23.8	81	17.56	5	37	204	
4					34	37.6	10	25.0	81	21.67	5.5	39	222	
5					44	42.8	15	28.4	81	24.04	8	40	221	
6					39	40.3	20	26.8	82	26.33	6.5	42	221	
7					40	40.8	25	27.1	82	28.59	7.5	42	220	
8					46	43.7	30	29.1	83	31.08	9.5	43	219	
9					50	45.6	35	30.3	84	33.63	10	44	222	
10					53	47.2	40	31.1	84	36.29	10.5	45	227	
11					55	48.1	45	31.6	85	38.93	11	42	230	
12					53	47.3	50	31.0	85	41.52	11	43	231	
							1680		82.8	23.94	8.45	41.7	221.7	
									542	19.8214			681	
23.51243														

Source Test Team
CHUCK McCURE
Source Test Engineer II

SPINNSBO
MAY 00 25 +
100 H

Condensate $\frac{V_o}{V_{H_2O}} \frac{S_{CF}}{S_{CF}}$

$$Q_m = \left[(2.638 \times 10^{-3}) \frac{V_g}{T_g} (100 - H_2O)^2 D_{\text{Hum}} \right] \quad (100 - H_2O)^2$$

$$V_s = (K)(C_P) \sqrt{\frac{T_s \cdot \Delta P}{29.98}}$$

$$V_s = \frac{17.71 (V_m)(P_b)}{I_{\text{torr}}} = 23.032 \text{ SCF}$$

list DETAIL for plant # >>
103

Plant number 103
Business name Kaiser Sand and Gravel
Location address 3311 Stanley Boulevard
City Pleasanton, CA 94566
Telephone (415) 846-8800
Mailing address P O Box 580
City Pleasanton, CA 94566
Principal product Asphaltic concrete
Parent company Koppers Co , Inc
Contact Larry Appleton
Title Project Coordinator
Address P O Box 580
City Pleasanton, CA 94566
Telephone (415) 846-8800
Permit engr, current ... J Julian Elliot (544)
Permit engr, former Hari S Doss (442)
Inspection Area # 805 - Christopher W Berglund (552)
Inspection Materials ... 02/08/91
Ownership type Private
Number of employees 3
Property area, acres ... 3
Inside city limits Yes
Permit month 10

list DETAIL for plant # >>

*Tom Jackson
933-6366*

REG 10

*P.C. 5/6-14 35-ME+Tom - WILL CALL W/ BUSY DAY!
P.C. 5/18 - 0920 - LEFT MESSAGE-TOM - PLEASE CALL.*

PLANT 103 Kaiser Sand and Gravel; Pleasanton

SOURCE 11 MINERL-DRY> Rotary dryer, Burns multi-fuels, 162MM BTU/hr max,
Asphaltic concrete, 350 tons/hr max

ASPHALT PLANT DRYER

Make, model: GENCO; Ultra Flame Mod.135,162E6 BTU

Primary Use: Other

External combustion: Dryer (non-foods)

GENCO FP-162 (ONE EACH)

Combustion products-

70000 cfm wet gas flow rate, 350 F

Subject to Reg: 10-7

P/O \$1871 Fee

Insp Freq: 12 mo

Emission train: @ >A10

Plant # >>

device	READ	"to"	ADVANCE	2400	13	ADVANCE	COPY	COPY	COPY
modes	DISK	devices	PAGE	CN		LINE	ALL	PAGE	LINE

PLANT#
103

Kaiser Sand and Gravel
3311 Stanley Boulevard
Pleasanton, CA 94566

Sources:

- 9 COLD AGGREGATE STORAGE
- 11 ASPHALT PLANT DRYER
- 12 CONVEYORS (ASPHALTIC CONCRETE AND AGGREGATE)
- 13 HOT ASPHALT STORAGE TANK
- 14 HOT ASPHALT STORAGE TANK
- 15 BLENDED FUEL TANK WASTE OIL AND DIESEL - .1 TO .2 SULFUR
- 16 ASPHALT CONCRETE STORAGE SILO
- 17 ASPHALT CONCRETE STORAGE SILO
- 18 ASPHALT CONCRETE STORAGE SILO
- 19 Cold Cleaner
- 20 Cold Cleaner
- 21 Cold Cleaner
- 22 Cold Cleaner
- 23 Cold Cleaner
- 24 Cold Cleaner
- 100 GASOLINE DISPENSING STATION

Abatement Devices:

- 10 DUAL CYCLONES
- 11 BAGHOUSE

Emission Points:

- 12 train: ,A11,/