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SB Co. APCD

MAY 25 1990

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GRANITE CONSTRUCTION
P.O. BOX 6744
GOLETA, Ca. 93111

COMPLIANCE TEST
ROTARY DRIER BAGHOUSE
MAY 8, 1990

SBCAPCD PERMIT TO OPERATE NUMBER
1957

Prepared By:

BTC ENVIRONMENTAL, INC.
1536 EASTMAN AVENUE
Ventura, CA 93003

Job Number
7019

Laboratory Report Number
A0-081

Test Team Leader
Mark Patrick

Results Verified By:
Tom Porter - Field Operations Manager
Matthew Pena - Division Manager

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EMISSION SUMMARY

CONSTITUENT	RUN #1	RUN #2	RUN #3	AVERAGE
Total Particulate				
gr/DSCF	0.0550 ✓	0.0350 ✓	0.0501 ✓	0.0467 ✓
lbs/hr	11.88 ✓	6.96 ✓	9.80 ✓	9.55 ✓

@ 12% CO₂ (gr/DSCF) ~~0.12% CO~~ 0.1245 0.0764 0.1078 0.1029

(ARB-100, Section 6.3)

emissions @ 200 tons/hr

11.88 lbs/hr	6.96	9.80
201 tons/hr	217 tons/hr	222 tons/hr

I. INTRODUCTION

SAMPLING AND ANALYTICAL PROCEDURES

On May 8, 1990, BTC Environmental performed source emissions tests for particulate matter on the Rotary Drier Baghouse located at Granite Construction in Buellton, California. The unit is natural gas fired to dry the aggregate prior to the mixing of the asphalt. The sampling was done on the exhaust stack of the baghouse.

The plant was operating at 201 tons/hour during the first run, 217 tons/hour during the second run and 222 tons/hour during the third run.

STACK GAS ANALYSIS: Samples of the stack gas were taken from the exhaust stack and analyzed for oxygen and carbon dioxide. The oxygen was determined by a Teledyne electrochemical cell oxygen analyzer. The carbon dioxide was checked using an ACS Fuji non-dispersive infrared analyzer. Readings were obtained continuously during each run and then averaged together to obtain the stack gas composition. The data was recorded on the run sheets at 6 minute intervals and on a strip chart recorder.

STACK GAS VELOCITY: The stack gas velocity was determined using an "S" type pitot tube connected to a magnehelic gauge. The "S" type pitot was used to determine the stack velocity profile for each run.

The stack temperature was determined using a thermocouple and an indicating pyrometer. The proportion of water was determined gravimetrically and the dry molecular weight of the stack gas determined by E.P.A. Method 3, equation 3-2. Stack velocities were calculated using E.P.A. Method 2, equation 2-9; gas volumetric flow rate was determined by equation 2-10.

PARTICULATE EMISSIONS: Particulates were collected isokinetically using a Lase Model 31 stack sampler system that conforms to E.P.A. requirements for particulate sampling. The system consists of a heated probe, heated filter, and cooled impingers (see E.P.A. Method 5). After the weight of the particulates on the filter and in the probe is determined, the total dissolved solids in the the impingers is determined and added to the particulate weight in order to comply with Santa Barbara County APCD regulations. Blanks for the DI water and acetone were analyzed and subtracted from the total particulate weight.

LEAK CHECKS: Leak rates were conducted on the sampling train and the pitot tubes before and after each test. The leak check for the sampling train was done at the nozzle.

All calculations for lb/hr were done by using the flow rate of the stack gas. All values were calculated by using Santa Barbara County APCD standard conditions (60°F & 29.92 in Hg).

If you have any questions concerning this test or if we can be of further assistance, please contact the undersigned at (805) 644-1095.

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If you have any questions concerning this test or if we can be of further assistance, please contact the undersigned at (805) 644-1095.

Respectfully submitted,

BTO Environmental, INC.



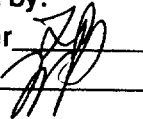
Tom Porter

Field Operations Manager

Reviewed by:

T. Porter

M. Pena



Copies: 3 Granite

1 File

II. WET TEST METHODS DATA SUMMARIES

FIELD DATA SUMMARY

Asphalt Baghouse

	Run#1	Run#2	Run#3
Vlc - Volume of water collected, ml	350.2	360.2	369.0
Vm - Gas volume, meter cond., dcf	39.385	42.435	39.179
Y - Meter calibration factor	0.941	0.941	0.941
Pbar - Barometric pressure, in. Hg	29.74	29.74	29.70
Pg - Stack static pressure, in. H2O	-0.40	-0.40	-0.40
ΔH - Avg. meter press. diff., in. H2O	1.067	1.078	0.980
Tm - Absolute meter temperature, °R	531.8	544.1	550.9
Vm(std) - Standard sample gas vol., dscf	36.1189	38.0408	34.6301
Bws - Water vapor part in gas stream	0.311	0.305	0.331
CO2 - Dry concentration, volume %	5.3	5.5	5.2
O2 - Dry concentration, volume %	11.5	10.9	11.1
Md - Mol wt. stack gas, dry, g/gmole	29.303	29.320	29.280
Ms - Mol wt. stack gas, wet, g/gmole	25.790	25.863	25.547
Cp - Pitot tube coef., dimensionless	0.843	0.830	0.843
Δp - Avg. of sq. roots of each Δp	0.873	0.816	0.815
Ts - Absolute stack Temp. °R	719.7	727.2	726.7
A - Area of stack, square feet	13.93	13.93	13.93
Qstd - Volumetric flow rate, dscfm	25200	23215	22815
An - Area of nozzle, square feet	0.0002786	0.0003012	0.0002786
ϕ - Sampling time, minutes	72	72	72
I - Isokinetic variation, percent	103.8 ✓	109.8 ✓	109.8 ✓

FIELD DATA & CALCULATIONS SUMMARY

Client: **Granite Construction**

Site: **Buellton**

Unit: **Asphalt Baghouse**

Date: **5/8/90**

Type: **T std = 60 F**

Run: **1**

Wc	Water Condensate Weight	350.2	g		
Vlc	Water Condensate Volume	350.8	ml		
Vm	Metered Sample Gas Volume	39.385	dcf		
Ip	Avg. Leak Rate	0.000	cf		
Vh	Leak Corrected Sample Gas Volume	39.385	dcf		
Y	Dry Gas Meter Calibration Factor	0.941			
Pbar	Barometric Pressure	29.74	In. Hg		
Pg	Static Pressure	-0.4	In. H2O		
Ps	Stack Pressure, Absolute	29.71	In. Hg		
Δ H	Dry Gas Meter Press. Differential, Average	1.067	In. H2O		
Tm	Dry Gas Meter Temperature, Average	71.8	deg. F	531.8	deg. R
Vm(std)	Sample Gas Volume	36.1189	dscf		
Vm(wet)	Sample Gas Volume, Wet	52.4096	scf		
Vw(std)	Water Vapor Volume	16.2907	scf		
Bws	Water Content of Stack Gas	0.311		31.1	%
CO2	Carbon Dioxide, Dry	5.3	%		
O2	Oxygen, Dry	11.5	%		
N2	Nitrogen, Dry	83.2	%		
Md	Molecular Wt. of Stack Gas, Dry	29.303	lb/lb mole		
Ms	Molecular Wt. of Stack Gas, Wet	25.790	lb/lb mole		
Cp	Pitot Calibration Factor	0.843			
Δ P	Velocity Head, Average Square Root	0.873	In. H2O		
Ts	Stack Gas Temperature, Average	259.7	deg. F	719.7	deg. R
As	Area of Stack	13.93	sq ft	50.5	in. dia.
Vs	Stack Gas Velocity	60.97	ft/sec		
Qa	Actual Flow Rate	50,964	cfm		
Qad	Actual Flow Rate, Dry	35,122	dcfm		
Q(std)	Stack Gas Flow Rate	25,200	dscfm		
An	Nozzle Area	0.0002786	sq ft	0.226	in. dia.
Theta	Sampling Time	72	min.		
I	Isokinetics	103.8	%		

FIELD DATA & CALCULATIONS SUMMARY

Client: **Granite Construction**
 Site: **Buellton**
 Unit: **Asphalt Baghouse**

Date: **5/8/90**
 Type: **T std = 60 F**
 Run: **2**

Wc	Water Condensate Weight	359.6 ✓	g ✓		
Vic	Water Condensate Volume	360.2 ✓	ml ✓		
Vm	Metered Sample Gas Volume	42.435 ✓	dcf		
Lp	Avg. Leak Rate	0.000	cf		
Vh	Leak Corrected Sample Gas Volume	42.435 ✓	dcf ✓		
Y	Dry Gas Meter Calibration Factor	0.941 ✓			
Pbar	Barometric Pressure	29.74 ✓	In. Hg		
Pg	Static Pressure	-0.4 ✓	In. H2O		
Ps	Stack Pressure, Absolute	29.71 ✓	in. Hg		
Δ H	Dry Gas Meter Press. Differential, Average	1.078 ✓	In. H2O		
Tm	Dry Gas Meter Temperature, Average	84.1 ✓	deg. F	544.1	deg. R
Vm(std)	Sample Gas Volume	38.0408 ✓	dscf		
Vm(wet)	Sample Gas Volume, Wet	54.7687 ✓	scf		
Vw(std)	Water Vapor Volume	16.7280 ✓	scf		
Bws	Water Content of Stack Gas	0.305 ✓		30.5	%
CO2	Carbon Dioxide, Dry	5.5 ✓	%		
O2	Oxygen, Dry	10.9 ✓	%		
N2	Nitrogen, Dry	83.6 ✓	%		
Md	Molecular Wt. of Stack Gas, Dry	29.320 ✓	lb/lb mole		
Ms	Molecular Wt. of Stack Gas, Wet	25.863 ✓	lb/lb mole		
Cp	Pitot Calibration Factor	0.830 ✓			
Δ P	Velocity Head, Average Square Root	0.816 ✓	In. H2O		
Ts	Stack Gas Temperature, Average	267.2 ✓	deg. F	727.2	deg. R
As	Area of Stack	13.93 ✓	sq ft	50.5	in. dia.
Vs	Stack Gas Velocity	56.31 ✓	ft/sec		
Qa	Actual Flow Rate	47,070 ✓	cfm		
Qad	Actual Flow Rate, Dry	32,693 ✓	dcfm		
Q(std)	Stack Gas Flow Rate	23,215 ✓	dscfm		
An	Nozzle Area	0.0003012 ✓	sq ft	0.235	in. dia.
Theta	Sampling Time	72 ✓	min.		
I	Isokinetics	109.8 ✓	%		

FIELD DATA & CALCULATIONS SUMMARY

Client: **Granite Construction**
 Site: **Buellton**
 Unit: **Asphalt Baghouse**

Date: **5/8/90**
 Type: **T std = 60 F**
 Run: **3**

Wc	Water Condensate Weight	368.3	g		
Vlc	Water Condensate Volume	369.0	ml		
Vm	Metered Sample Gas Volume	39.179	dcf		
Lp	Avg. Leak Rate	0.000	cf		
Vh	Leak Corrected Sample Gas Volume	39.179	dcf		
Y	Dry Gas Meter Calibration Factor	0.941			
Pbar	Barometric Pressure	29.70	In. Hg		
Pg	Static Pressure	-0.4	In. H2O		
Ps	Stack Pressure, Absolute	29.67	in. Hg		
Δ H	Dry Gas Meter Press. Differential, Average	0.980	In. H2O		
Tm	Dry Gas Meter Temperature, Average	90.9	deg. F	550.9	deg. R
Vm(std)	Sample Gas Volume	34.6301	dscf		
Vm(wet)	Sample Gas Volume, Wet	51.7628	scf		
Vw(std)	Water Vapor Volume	17.1327	scf		
Bws	Water Content of Stack Gas	0.331		33.1	%
CO2	Carbon Dioxide, Dry	5.2 ✓	% ✓		
O2	Oxygen, Dry	11.1 ✓	% ✓		
N2	Nitrogen, Dry	83.7 ✓	%		
Md	Molecular Wt. of Stack Gas, Dry	29.280	lb/lb mole		
Ms	Molecular Wt. of Stack Gas, Wet	25.547	lb/lb mole		
Cp	Pitot Calibration Factor	0.843			
Δ P	Velocity Head, Average Square Root	0.815	In. H2O		
Ts	Stack Gas Temperature, Average	266.7	deg. F ✓	726.7	deg. R
As	Area of Stack	13.93 ✓	sq ft	50.5	in. dia.
Vs	Stack Gas Velocity	57.49	ft/sec		
Qa	Actual Flow Rate	48,056	cfm		
Qad	Actual Flow Rate, Dry	32,150	dcfm		
Q(std)	Stack Gas Flow Rate	22,815	dscfm		
An	Nozzle Area	0.0002786	sq ft	0.226	in. dia.
Theta	Sampling Time	72	min.		
I	Isokinetics	109.8	%		

BTC ENVIRONMENTAL
EPA methods 2, 3, 4, 5, 6, 8

CONSTANTS & CONVERSIONS

Tstd = 60, 68, or 70 °F	1 in. Hg = 13.6 in. H ₂ O
Pstd = 29.92 in. Hg	1 lb = 453.6 g
R = 21.85(in. Hg-cu ft/lb mole-°R)	1 lb = 7000 grain
Dw = 0.9982(g/ml)	1 g = 15.432 grain
MW(H ₂ O) = 18.0 lb/lb mole	1 mg = 0.001 g
MW(Sulfur) = 32.03 lb/lb mole	1 hr = 60 min.
M(H ₂ SO ₄) = 98.08 lb/lb mole	1 part/vol X = 1*10 ⁶ ppmv X
MW(SO ₂) = 64.06 lb/lb mole	1 bbl = 42 gal
K(H ₂ SO ₄) = 0.5 mg-g mole/g-meq	M = 1000
K(SO ₂) = 0.5 mg-g mole/g-meq	La = 0.02 cfm
Kp = 85.49(ft/sec(sqrt(lb/lb mole-in.Hg/°R-in. H ₂ O)))	
Kw,[cu ft/g-°R] = R / (453.6*MW(H ₂ O)*Pstd)	
Kf,[scf-ppm/lb mole] = R * (Tstd+460) * (1*10 ⁶) / Pstd	

INTERMEDIATE CALCULATIONS

$$F_{\text{[scf/MMBtu]}} = F \text{ Factor} * (T_{\text{std}} + 460) / 528$$

$$Ph_{\text{[in. Hg]}} = P_{\text{bar}} + (\Delta H / 13.6)$$

$$N_2\text{[%]} = 100 - (O_2\% + CO_2\%)$$

$$Vlc_{\text{[ml]}} = Ww / Dw$$

$$Qa_{\text{[cfm]}} = 60 * Vs * As$$

$$Qad_{\text{[dcfm]}} = Qa * (1 - Bws)$$

CFR 40 - EPA EQUATIONS

eq. 2-8 $T[°R] = T[°F] + 460$

eq. 2-6 $Ps_{\text{[in. Hg]}} = P_{\text{bar}} + (Pg/13.6)$

eq. 5-3 $Bws_{\text{[%]}} = Vw(\text{std}) / \{ Vw(\text{std}) + Vm(\text{std}) \}$

eq. 3-2 $Md_{\text{[lb/lb-mole]}} = 0.44*CO_2\% + 0.32*O_2\% + 0.28*(N_2\% + CO\%)$

eq. 2-5 $Ms_{\text{[lb/lb mol]}} = Md*(1-Bws) + (MW(H_2O)*Bws)$

eq. 5-2 $Vw(\text{std})_{\text{[scf]}} = Ww * Kw * (T_{\text{std}} + 460)$

eq. 5-1 $Vn_{\text{[cf]}} = Vm - ((Lp-La) * Theta)$

eq. 5-1 $Vm(\text{std})_{\text{[sdcf]}} = Vm * Y * ((T_{\text{std}} + 460) / (Tm + 460)) * Ph / Pstd$

eq. 2-9 $Vs_{\text{[ft./sec.]}} = Kp * Cp * (\Delta P * (Ts + 460) / (Ps * Ms))^{0.5}$

eq. 2-10 $Qstd_{\text{[dscfm]}} = Qad * (T_{\text{std}} + 460) * Ps / ((Ts + 460) * Pstd)$

eq. 5-8 $I_{\text{[%]}} = 100 * (Ts + 460) * Vm(\text{std}) * Pstd / (60 * Vs * Theta * An * Ps * (1 - Bws) * (T_{\text{std}} + 460))$

eq. 5-6 $Cx_{\text{[grain/dscf]}} = Wx_g * 15.432 / Vm(\text{std})$

eq. 8-2,3 $Wx_{\text{[mg]}} = (Vt - Vtb) * N(\text{std}) * (Vsoln / Valq) * MWx * Kx$

$Cx_{\text{[grain/dscf]}} = Wx_{\text{mg}} * 0.001 * 15.432 / Vm(\text{std})$

$CWx_{\text{[grain/scf]}} = Cx * (1 - Bws)$

$CCx_{\text{[grain/dscf @ 12\% CO}_2\text{]}} = Cx * 12.0 / CO_2\%$

$CWCx_{\text{[grain/scf @ 12\% CO}_2\text{]}} = CCx$

$CPx_{\text{[ppmv dry]}} = Cx * Kf / (MWx * 7000)$

$CPCx_{\text{[ppmv @ N\% O}_2\text{]}} = CPx * ((20.9 - N\%) / (20.9 - O_2\%))$

$CFx_{\text{[lb/hr]}} = Cx * Q(\text{std}) * 60 / 7000$

$CEx_{\text{[lb/MMBtu]}} = F * (Cx / 7000) * (20.9 / (20.9 - O_2\%))$

$CBx_{\text{[lb/bbl]}} = CEx * (Fuel \text{ Btu/MM}) * (Fuel \text{ lb/gal}) * 42$

$CEsx_{\text{[lb S/MMBtu]}} = CEx * (MW(S) / MWx)$

Where x represents, Particulate, Sulfuric Acid, Sulfate, or Sulfur Dioxide respectively.

III. WET TEST METHODS CALCULATIONS

CALCULATED EMISSION RESULTS

Client: Granite Construction
Site: Buellton
Unit: Asphalt Baghouse

Date: 5/8/90
Type: T std = 60 F
Run: 1

Total Particulate

Ws	Particulate Weight	0.1287	g
Cs	Particulate Emissions	0.0550	grain/dscf
CFs	Particulate Flow Rate	11.88	lb/hr

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CALCULATED EMISSION RESULTS

Client: Granite Construction
Site: Buellton
Unit: Asphalt Baghouse

Date: 5/8/90
Type: T std = 60 F
Run: 2

Total Particulate

Ws	Particulate Weight	0.0862 ✓	g ✓
Cs	Particulate Emissions	0.0350 ✓	grain/dscf ✓
CFs	Particulate Flow Rate	6.96 ✓	lb/hr

BTC Environmental, Inc. - 1989

CALCULATED EMISSION RESULTS

Client: **Granite Construction**
Site: **Buellton**
Unit: **Asphalt Baghouse**

Date: **5/8/90**
Type: **T std = 60 F**
Run: **3**

Total Particulate

Ws	Particulate Weight	0.1125	g
Cs	Particulate Emissions	0.0501	grain/dscf
CFs	Particulate Flow Rate	9.80	lb/hr

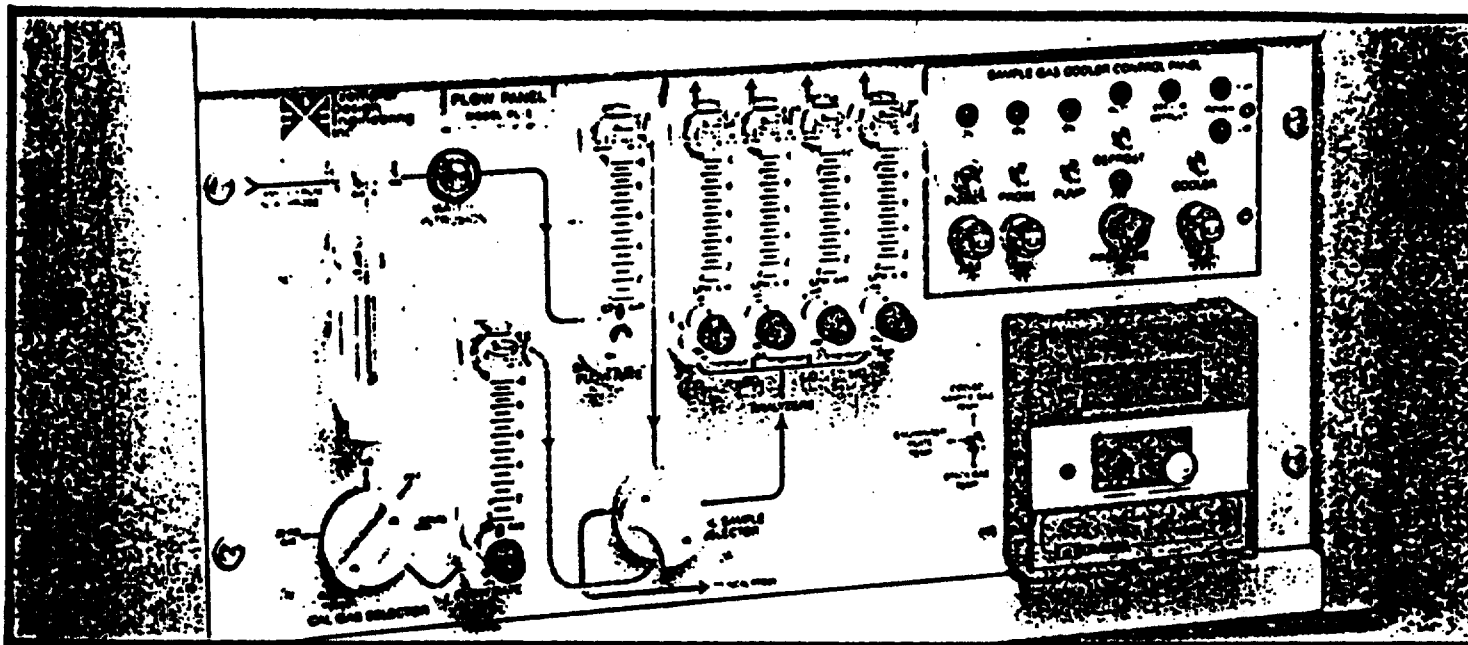
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IV. CONTINUOUS TEST METHODS DATA

Extractive Gas Sampling System

Model EGS-1 (Patent Applied For)

Exemplar's Extractive Gas Sampling System, Model EGS-1 is specifically designed to be a complete, easy to use, portable extractive gas sampling system for use with continuous gas analyzers. By combining individual Exemplar components, a complete system requires only the addition of user specified analyzers and calibration gases. The system is easy to operate and difficult to mis-calibrate.

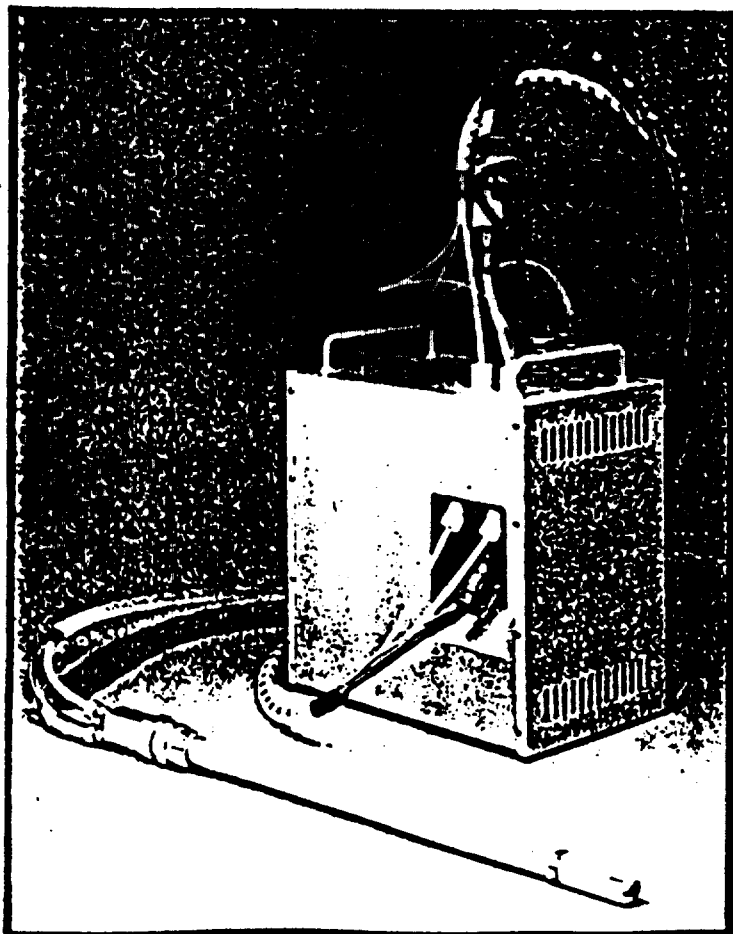


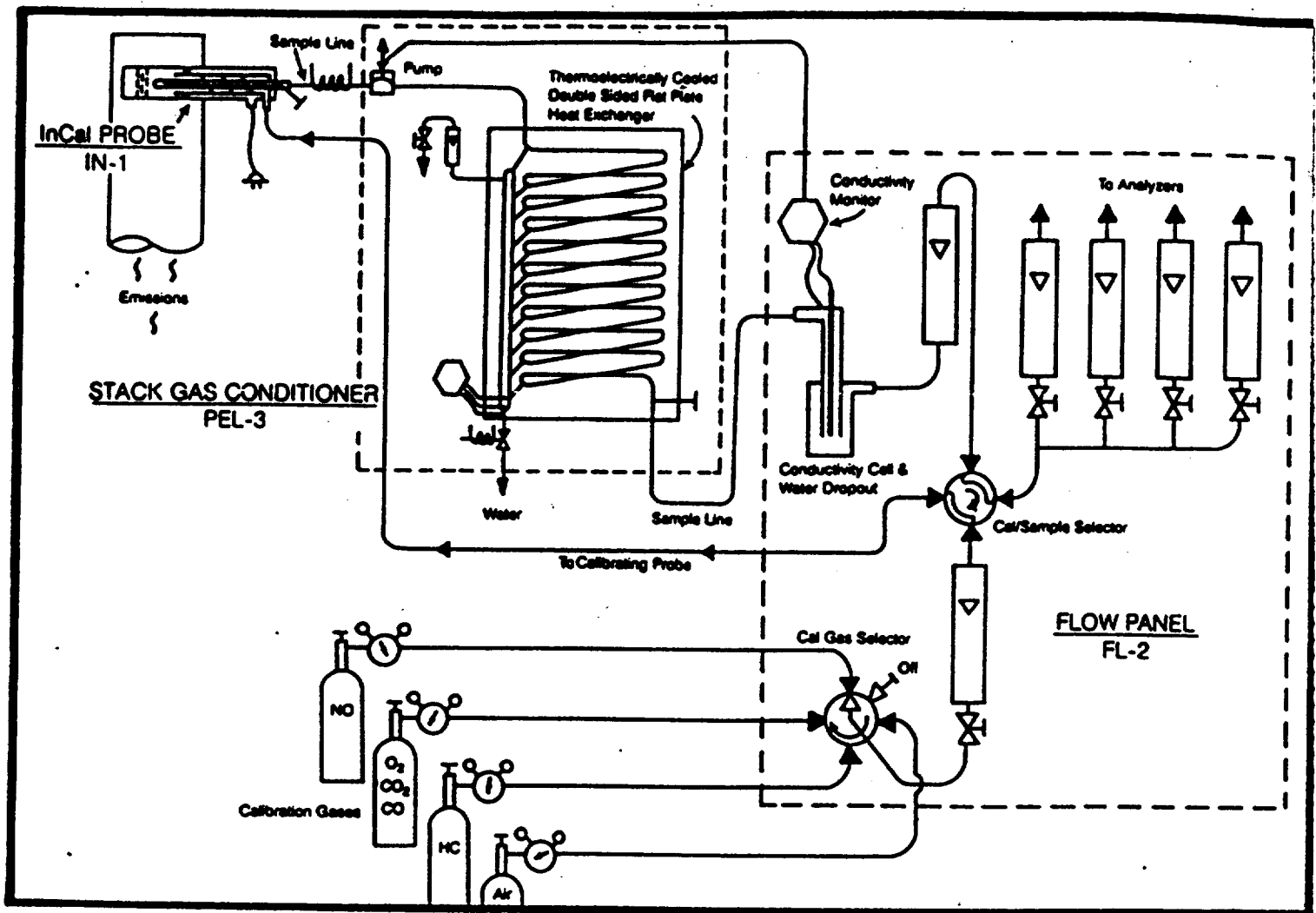
SPECIAL FEATURES

- Simple to use; only requires connecting to analyzers, cal gases and electrical power.
- Easily portable; system, analyzers and cal gases will fit into and operate from the back of a standard station wagon.
- Highly accurate; both internal and external calibration from probe tip, system is easy to calibrate.
- High capacity and non-scrubbing; powerful thermoelectric coolers with special heat exchanger design removes condensing water as quickly as it is formed.
- Positive pressure design; eliminates concentration errors due to leaks.
- Corrosion and reaction resistant; sample contacts only non-reactive, non-absorbing materials.

APPLICATIONS

- Use where EPA extractive sampling requirements are specified.
- Use where high accuracy is essential.
- Replace older, complex negative pressure systems.
- Complete extractive system without the need for a sampling van.
- Use where space is limited.



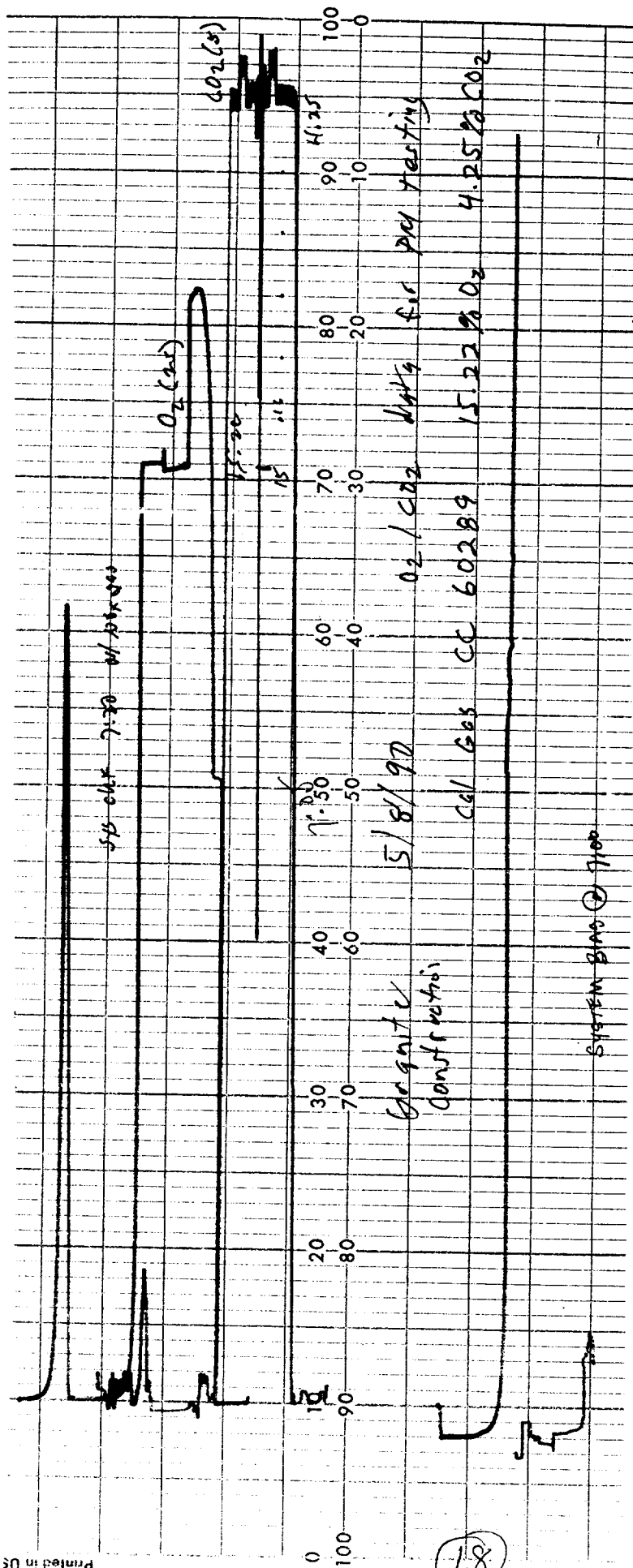


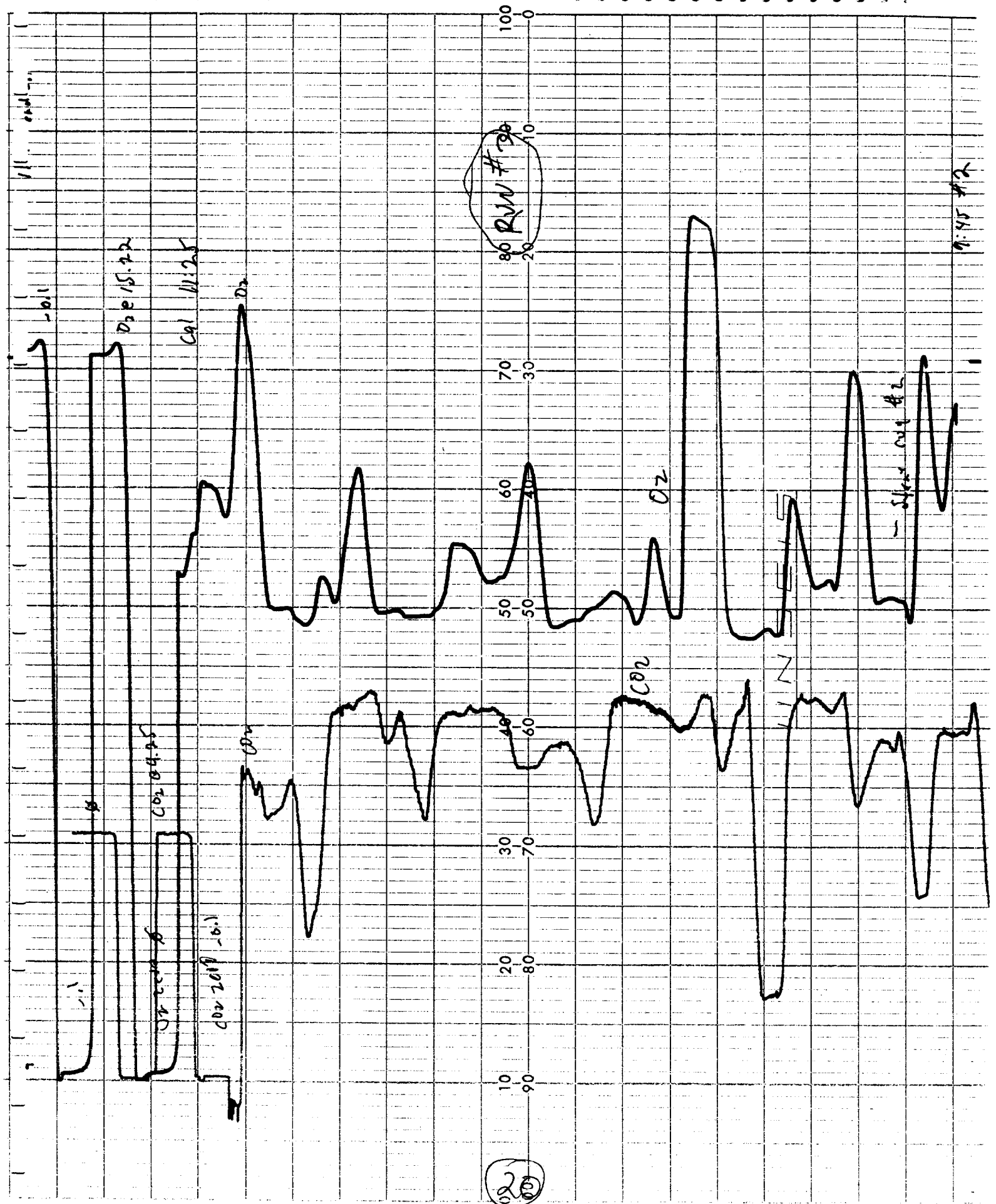
Components

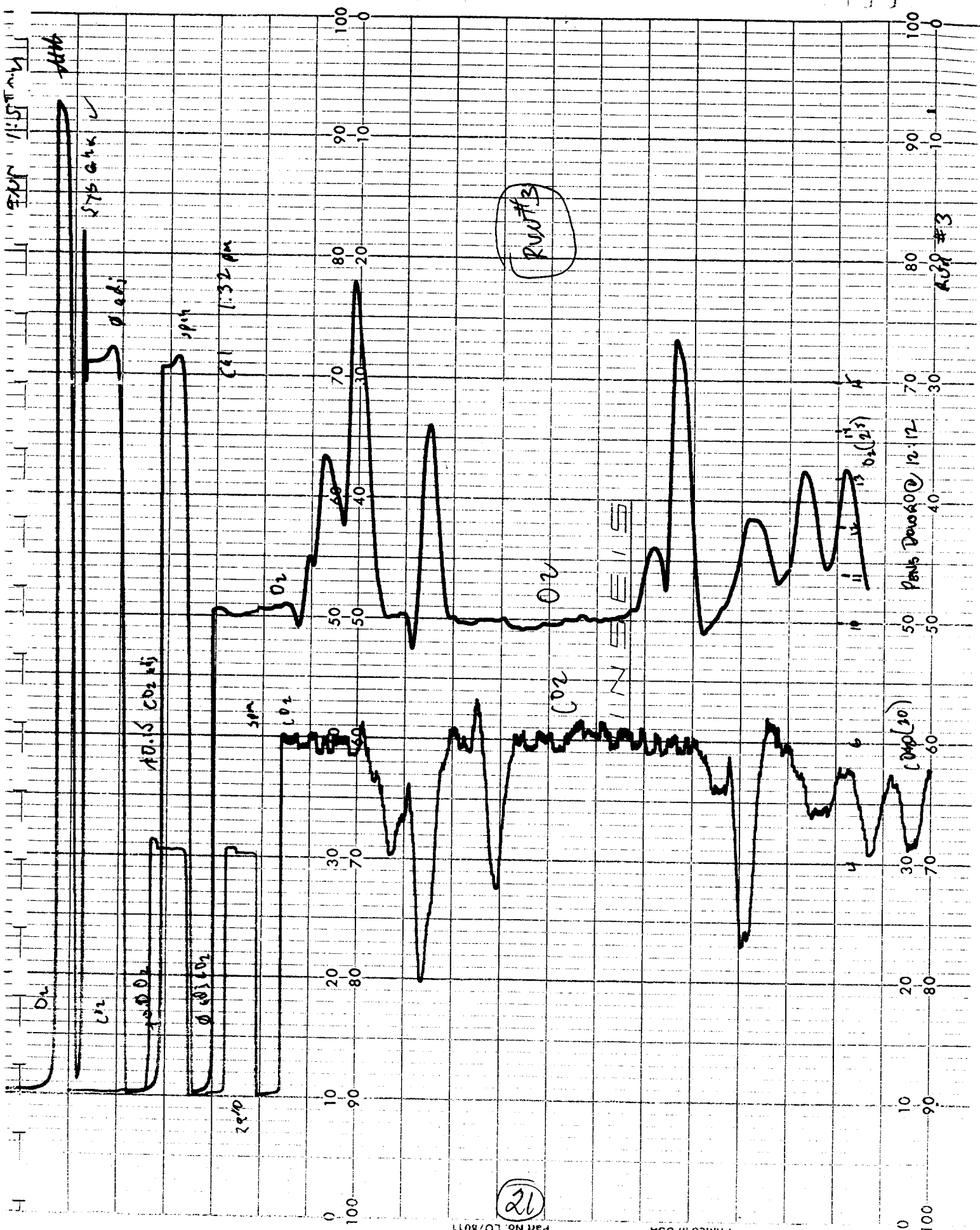
Exemplar's InCal IN-1 series of in-stream calibrating probes are used to provide filtered non-condensing sample gas from a wide range of sources. The probe's in-stream calibration feature allows the entire system (probe tip to analyzer) to be accurately calibrated. The probe's design, size and corrosion resistance make sample extraction easy.

Exemplar's Sample Gas Conditioner PEL-3 provides the distribution panel with sample gas under positive pressure. A vibrating armature pump followed by a double sided, thermoelectrically cooled, flat plate heat exchanger with integral water separation channels, is capable of producing 5 lpm of 40°F dew point sample gas from a 160°F, water saturated (30%) sample stream. The condensing water dump is automatic allowing for continuous operation. The positive pressure nature of the system eliminates sample dilution due to tube fitting leaks. The unit is light weight and easily portable.

Exemplar's Sample Distribution Flow Panel FL-2 distributes dry, positive pressure, non-scrubbed sample gas to the appropriate instruments. The panel allows for both internal and probe tip calibration. Manual, click stop, rotary plug valves and an illustrative front panel provide leak free, fail-safe sample and calibration gas distribution. Flow paths are simple and easy to understand. This unit is small and easily transportable.







V. LABORATORY ANALYSIS

Run Set Up Sheet

Client : Granite Construction
 Site : Buellton
 Unit: Asphalt Baghouse

Date : 5/8/90
 Job #: -
 Lab #: A0-081

Method#: 5
 Run#: 1
 Hot box#: -

Probe#: 2
 Stack box#: B
 Cold box#: 3

Pryo#: -
 Nozzle#: 0.226
 Pitot#: 0.843

Imp. #1:

gross	837.9
tare	617.8
final	220.1

Imp. #2:

gross	758.7
tare	631.3
final	127.4

Imp. #3:

gross	468.6
tare	465.1
final	3.5

Imp. #4:

gross	652.5
tare	653.3
final	-0.8

Total 350.2

Probe blank

--

 ml
 Probe rinse

--

 ml

Solution blank

Acetone

 Solution blank

DI Water

Filter No:

C-15

 Filter Tare wt.

--

	#	date
Solution Container		
Solution Container		

Sample Vol:

start	150.0
Imp#1	finsh

 ml
 Amount Gained: 220.0 ml

Sample Vol:

start	150.0
Imp #2	finsh

 ml
 Amount Gained: 122.0 ml

Total Vol #1 #2 & Rinse 500.0 ml

Comments: _____

Run Set Up Sheet

Client : Granite Construction
 Site : Buellton
 Unit: Asphalt Baghouse

Date : 5/8/90
 Job #: -
 Lab #: A0-081

Method#: 5
 Run#: 2
 Hot box#: -

Probe#: 7
 Stack box#: B
 Cold box#: 2

Pryo#: -
 Nozzle#: 0.235 ✓
 Pitot#: 0.830 ✓

Imp. #1:

gross	858.2
tare	620.6
final	237.6

 ✓

Imp. #2:

gross	701.9
tare	590.2
final	111.7

 ✓

Imp. #3:

gross	486.0
tare	482.1
final	3.9

 ✓

Imp. #4:

gross	632.5
tare	626.1
final	6.4

 ✓

Total 359.6 ✓

Probe blank

--

 ml
 Probe rinse

--

 ml

Solution blank Acetone
 Solution blank DI Water

Filter No: C-17
 Filter Tare wt.

--

	#	date
Solution Container		
Solution Container		

Sample Vol:

start	150.0
finsh	388.0

 ml
 Imp#1
 Amount Gained: 238.0 ml

Sample Vol:

start	150.0
finsh	262.0

 ml
 Imp #2
 Amount Gained: 112.0 ml

Total Vol #1 #2 & Rinse 500.0 ml

Comments: _____

Run Set Up Sheet

Client : Granite Construction
 Site : Buellton
 Unit: Asphalt Baghouse

Date : 5/8/90
 Job #: -
 Lab #: A0-081

Method#: 5
 Run#: 3
 Hot box#: -

Probe#: 2
 Stack box#: B
 Cold box#: 6

Pryo#: -
 Nozzle#: 0.226
 Pitot#: 0.843

Imp. #1:

gross	841.1
tare	620.2
final	220.9

Imp. #2:

gross	767.2
tare	627.4
final	139.8

Imp. #3:

gross	469.8
tare	465.3
final	4.5

Imp. #4:

gross	655.6
tare	652.5
final	3.1

Total 368.3

Probe blank

--

 ml
 Probe rinse

--

 ml

Solution blank

Acetone

 Solution blank

DI Water

Filter No:

C-18

 Filter Tare wt.

--

	#	date
Solution Container		
Solution Container		

Sample Vol:

start	150.0
Imp#1	finsh

 ml
 Amount Gained: 221.0 ml

Sample Vol:

start	150.0
Imp #2	finsh

 ml
 Amount Gained: 140.0 ml

Total Vol #1 #2 & Rinse 500.0 ml

Comments: _____

PARTICULATE WEIGHTS : DATA & CALCULATIONS

Client : Granite Construction
 Site : Buellton
 Unit : Asphalt Baghouse

Run #: 1
 Box #: 3
 Filter #: C-15

Date : 5/8/90
 Job #: -
 Lab #: A0-081

SOLUTION BLANKS

Acetone -	Gross: <u>65.6941</u> g	Tare: <u>65.6928</u> g	Volume: <u>100</u> ml
			Residue: <u>0.0013</u> g
Alcohol -			Volume: <u>NA</u> ml
(80% ISO)	Gross: <u>NA</u> g	Tare: <u>NA</u> g	Residue: <u>NA</u> g
Freon -			Volume: <u>NA</u> ml
	Gross: <u>NA</u> g	Tare: <u>NA</u> g	Residue: <u>NA</u> g
DI Water -			Volume: <u>100</u> ml
	Gross: <u>67.5507</u> g	Tare: <u>67.5488</u> g	Residue: <u>0.0019</u> g
Probe -			Volume: <u>NA</u> ml
	Gross: <u>NA</u> g	Tare: <u>NA</u> g	Residue: <u>NA</u> g
		(less DI blank) =	Net: <u>NA</u> g

WEIGHTS & VOLUMES

A : Filter Catch - (C-15)

Gross: <u>0.4728</u> g	Tare: <u>0.4095</u> g	Net: <u>0.0633</u> g
------------------------	-----------------------	----------------------

C : Probe Catch -

Probe Blank:

Acetone: <u>75</u> ml	* <u>1.3E-05</u> g/ml	<u>0.0000</u> g
DI Water: <u>125</u> ml	* <u>1.9E-05</u> g/ml	<u>-0.0010</u> g
Gross: <u>70.4060</u> g	Tare: <u>70.3758</u> g	<u>-0.0024</u> g
		<u>0.0302</u> g
		Net: <u>0.0269</u> g

E : Impinger Catch -

DI Water: <u>300</u> ml	* <u>1.9E-05</u> g/ml	<u>-0.0057</u> g
Alcohol : <u>NA</u> ml	* <u>NA</u> g/ml	<u>0.0000</u> g
Total: <u>500</u> ml	Aliquot: <u>500</u> ml	
Gross: <u>72.7483</u> g	Tare: <u>72.7040</u> g	<u>0.0443</u> g
		Net: <u>0.0386</u> g

G : Organic Extract -

Freon: <u>NA</u> ml	* <u>NA</u> g/ml	<u>0.0000</u> g
Gross: <u>NA</u> g	Tare: <u>NA</u> g	<u>0.0000</u> g
		Net: <u>0.0000</u> g

Total Particulate Weight, (A+C+E+G) = 0.1287 g

PARTICULATE WEIGHTS : DATA & CALCULATIONS

Client : Granite Construction
 Site : Buellton
 Unit : Asphalt Baghouse

Run #: 2
 Box #: 2
 Filter #: C-17

Date : 5/8/90
 Job #: -
 Lab #: A0-081

SOLUTION BLANKS

Acetone -	Gross: <u>65.6941</u> g	Tare: <u>65.6928</u> g	Volume: <u>100</u> ml
			Residue: <u>0.0013</u> g
Alcohol -			Volume: <u>NA</u> ml
(80% ISO)	Gross: <u>NA</u> g	Tare: <u>NA</u> g	Residue: <u>NA</u> g
Freon -			Volume: <u>NA</u> ml
	Gross: <u>NA</u> g	Tare: <u>NA</u> g	Residue: <u>NA</u> g
DI Water -			Volume: <u>100</u> ml
	Gross: <u>67.5507</u> g	Tare: <u>67.5488</u> g	Residue: <u>0.0019</u> g
Probe -			Volume: <u>NA</u> ml
	Gross: <u>NA</u> g	Tare: <u>NA</u> g	Residue: <u>NA</u> g
		(less DI blank) =	Net: <u>NA</u> g

WEIGHTS & VOLUMES

A : Filter Catch - (C-17)

Gross: <u>0.4465</u> g	Tare: <u>0.4060</u> g	Net: <u>0.0405</u> g
------------------------	-----------------------	----------------------

C : Probe Catch -

Probe Blank:

Acetone: <u>75</u> ml	* <u>1.3E-05</u> g/ml	<u>0.0000</u> g
DI Water: <u>125</u> ml	* <u>1.9E-05</u> g/ml	<u>-0.0010</u> g
Gross: <u>70.4395</u> g	Tare: <u>70.4028</u> g	<u>-0.0024</u> g
		<u>0.0367</u> g
		Net: <u>0.0333</u> g

E : Impinger Catch -

DI Water: <u>300</u> ml	* <u>1.9E-05</u> g/ml	<u>-0.0057</u> g
Alcohol : <u>NA</u> ml	* <u>NA</u> g/ml	<u>0.0000</u> g
Total: <u>500</u> ml	Aliquot: <u>500</u> ml	
Gross: <u>68.9110</u> g	Tare: <u>68.8929</u> g	<u>0.0181</u> g
		Net: <u>0.0124</u> g

G : Organic Extract -

Freon: <u>NA</u> ml	* <u>NA</u> g/ml	<u>0.0000</u> g
Gross: <u>NA</u> g	Tare: <u>NA</u> g	<u>0.0000</u> g
		Net: <u>0.0000</u> g

Total Particulate Weight, (A+C+E+G) = 0.0862 g

PARTICULATE WEIGHTS : DATA & CALCULATIONS

Client : Granite Construction
 Site : Buellton
 Unit : Asphalt Baghouse

Run #: 3
 Box #: 6
 Filter #: C-18

Date : 5/8/90
 Job #: -
 Lab #: A0-081

SOLUTION BLANKS

Acetone -	Gross: <u>65.6941</u> g	Tare: <u>65.6928</u> g	Volume: <u>100</u> ml
			Residue: <u>0.0013</u> g
Alcohol -			Volume: <u>NA</u> ml
(80% ISO)	Gross: <u>NA</u> g	Tare: <u>NA</u> g	Residue: <u>NA</u> g
Freon -			Volume: <u>NA</u> ml
	Gross: <u>NA</u> g	Tare: <u>NA</u> g	Residue: <u>NA</u> g
DI Water -			Volume: <u>100</u> ml
	Gross: <u>67.5507</u> g	Tare: <u>67.5488</u> g	Residue: <u>0.0019</u> g
Probe -			Volume: <u>NA</u> ml
	Gross: <u>NA</u> g	Tare: <u>NA</u> g	Residue: <u>NA</u> g
		(less DI blank) =	Net: <u>NA</u> g

WEIGHTS & VOLUMES

A : Filter Catch - (C-18)

Gross: <u>0.4502</u> g	Tare: <u>0.4039</u> g	Net: <u>0.0463</u> g
------------------------	-----------------------	----------------------

C : Probe Catch -

Probe Blank:

Acetone: <u>75</u> ml * <u>1.3E-05</u> g/ml	<u>0.0000</u> g
DI Water: <u>125</u> ml * <u>1.9E-05</u> g/ml	<u>-0.0010</u> g
Gross: <u>72.9850</u> g	<u>-0.0024</u> g
Tare: <u>72.9543</u> g	<u>0.0307</u> g
	Net: <u>0.0273</u> g

E : Impinger Catch -

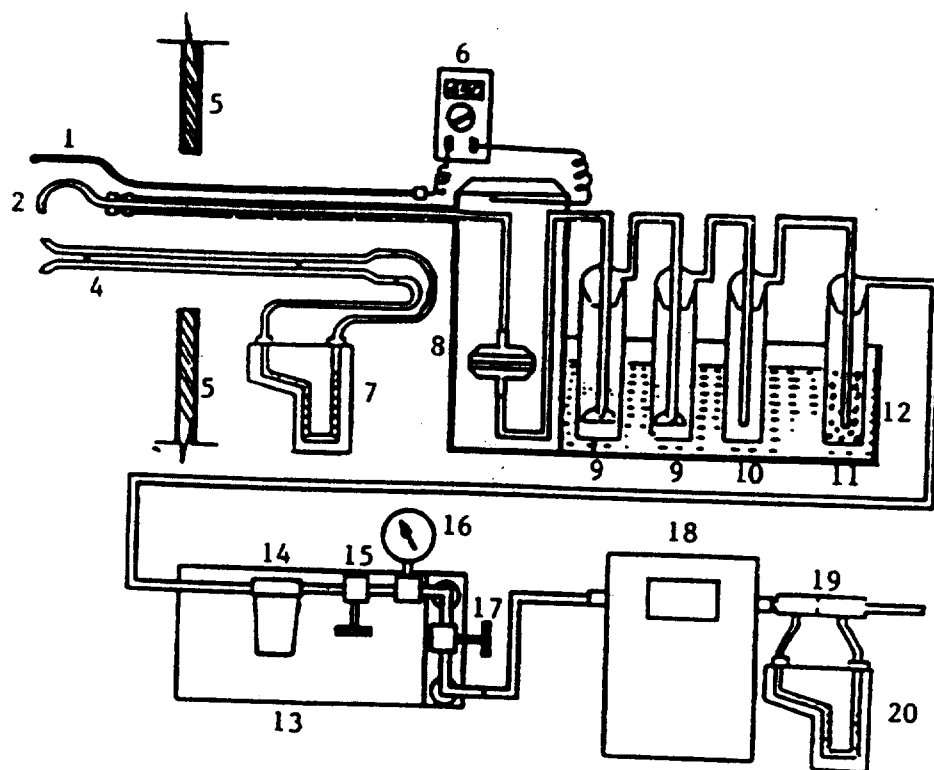
DI Water: <u>300</u> ml * <u>1.9E-05</u> g/ml	<u>-0.0057</u> g
Alcohol : <u>NA</u> ml * <u>NA</u> g/ml	<u>0.0000</u> g
Total: <u>500</u> ml	Aliquot: <u>500</u> ml
Gross: <u>71.6617</u> g	Tare: <u>71.6171</u> g
	<u>0.0446</u> g
	Net: <u>0.0389</u> g

G : Organic Extract -

Freon: <u>NA</u> ml * <u>NA</u> g/ml	<u>0.0000</u> g
Gross: <u>NA</u> g	Tare: <u>NA</u> g
	<u>0.0000</u> g
	Net: <u>0.0000</u> g

Total Particulate Weight, (A+C+E+G) = 0.1125 g

VI. METHODOLOGY



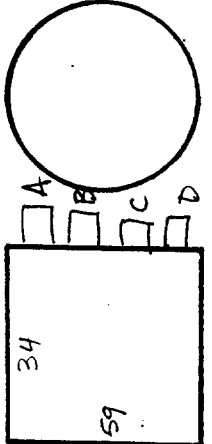
- | | |
|---|---|
| 1. Temperature Sensor | 11. Bubbler with Silica Gel |
| 2. Nozzle | 12. Ice Bath |
| 3. Glass lined Stainless Steel Probe-Heated | 13. Sealed Pump (Leak Free) |
| 4. S-type Pitot Tube | 14. Filter for Pump |
| 5. Stack Wall | 15. Metering Valve |
| 6. Temperature Sensor Meter | 16. Vacuum Gauge |
| 7. Pitot Tube Inclined Manometer | 17. By-pass Valve |
| 8. Heated Box with Filter | 18. Temperature Compensated Dry Gas Meter |
| 9. Impinger with 100 ml H ₂ O | 19. Orifice |
| 10. Empty Bubbler | 20. Orifice Inclined Manometer |

Figure 5.2-1
Particulate Sampling Train Set-up with
Heated Probe and Heated Filter

VII. RAW DATA

PLANT: Waukegan LOCATION: Refinery DATE: 5/8/70 RUN NO.: 1 (cont'd) SAMPLE BOX NO.: old box #3 METER BOX NO.: B PITOT FACTOR: #2, CR = .8428 METER FACTOR: VC = 19411, AHO = 20255 FILTER NO.: C-15

STACK CROSS SECTION



STATIC PRES -0.4 "H₂O" DRI-RITE WT.: "Hg

BAROMETRIC PRESS., IN. HG: 29.74 ASSUMED MOISTURE, %: 28.2 HEATER BOX SETTING: H₇ PROBE LENGTH, FT.: 5 NOZZLE DIAMETER, IN.: #22, 0.226" dia PROBE HEATER SETTING: H₇ APPROX. WIND VEL., MPH: 0 SAMPLE BOX TEMP., °F: 227

TRAVERSE POINT NUMBER	DISTANCE INCHES	O ₂ (%)	CO ₂ (%)	SAMPLE TIME MIN	STACK TEMP. (TS), °F	VELOCITY HEAD IN. H ₂ O		PRESSURE DIFF. ORIFICE METER (ΔH), IN. H ₂ O	DRY GAS SAMPLE VOLUME (VM), FT. ³	GAS SAMPLE TEMP. & DRY GAS METER		PUMP VACUUM IN. HG	TEMP. OF GAS FROM LAST IMP. °F
						AP	√AP			INLET (TM), °F	OUTLET (TM), °F		
C-1	2.8	10.6	5.7	0	248	0.7		0.97	582.103	74	73		
2	8.5	11.0	5.4	3	268	1.0		1.35	83.7	77	72		
3	14.2	10.8	5.4	6	272	1.1		1.48	85.6	79	72		
4	19.9	11.0	5.4	9	273	1.2		1.61	87.6	80	73	11	58
5	25.6	13.5	4.0	12	265	1.5		2.04	89.7	81	74	15	
6	31.3	12.5	4.6	15	260	1.3		1.91	91.9	81	75		
				18					594.488				
A-1	2.8	9.8	6.1	9:03	247	0.1		0.14		74	74	3	39
2	8.5	10.8	5.8	3	246	0.1		0.14	5.2	74	74		
3	14.2	11.5	5.2	6	267	0.5		0.67	5.8	74	74		
4	19.9	10.5	5.8	9	274	0.8		1.08	96.8	77	73	8	
5	25.6			12	278	0.8		1.06	8.5	78	73	9	
6	31.3			15	282	0.8		1.06	600.2	78	73		
AVERAGE	ZERO	0	0	18					601.995				
AVERAGE	SPAN	+2.2	0	72	259.7			0.873	39.385	AVG. 71.8			

PITOT LEAK CHECK: 11.5 5.3

BEFORE TOP ΔP = BOTTOM ΔP =

AFTER TOP ΔP = BOTTOM ΔP =

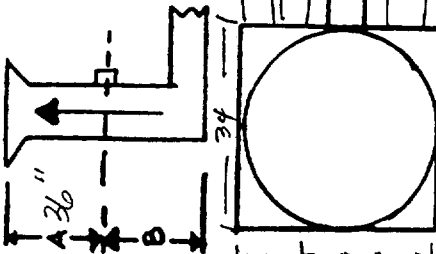
SAMPLE TRAIN LEAK CHECK:

BEFORE = CFM @ IN. HG

AFTER = CFM @ IN. HG

COMMENTS: PURGE

PLANT: Granite
 LOCATION: Buc 142
 COUNTY: Santa Barbara
 UNIT: 5/8/90
 DATE: 2
 RUN NO./METHOD: 2
 COLD BOX NO.: B
 METER BOX NO.: 7
 METER FACTOR: 9411 $\Delta H/D = 2.025$
 PITOT #/FACTOR: 7 $C_p = 0.8299$
 PYROMETER #: 1.1
 MAGNETIC FACTOR: ΔP M2 ΔH M4



FILTER NO.: C-17
 AMBIENT TEMP.: 71
 BAROMETRIC PRESS., IN. HG.: 29.74
 ASSUMED MOISTURE: 28%
 HEATER BOX SETTING: 45
 PROBE LENGTH, FT.: 5'
 NOZZLE DIAMETER, IN.: #24, 0.235" dia
 PROBE HEATER SETTING: 175
 APPROX. WIND VEL., MPH: 0
 SAMPLE BOX TEMP., (F): 220
 STATIC PRESSURE: -0.4 "H2O
 OFFSET: in. PORT DIA.: in.

$P_{static} = 29.7$
 (M / F)

TRAVERSE POINT NUMBER	DISTANCE INCHES	O2 (%)	CO2 (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY IN. H2O		PRESSURE DIFF ORIFICE METER (ΔH)	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GAS METER		PUMP VACUUM IN. HG	TEMP. LAST IMPINGER (F)
						ΔP	ΔP			INLET (Tm),	OUTLET (Tm)		
A-1	2.8	10.3	5.9	9:57	265	0.3		0.45	602.276	72	72	4	
2	8.5	13.5	4.0	3	251	0.1		0.15	3.3	74	71		
3	14.2	10.8	5.6	6	260	0.2		0.31	4.0	74	72		
4	19.9	11.3	5.2	9	270	0.5		0.17	5.0	78	72		
5	25.6	9.5	6.6	12	274	0.7		1.07	6.4	80	73		
6	31.3	9.5	6.4	15	278	0.8		1.22	8.1	82	74		
C-1	2.8	10.0	6.4	10:22		0.7		FINAL	607.857				
2	8.5	10.5	6.0	0	252	1.0		1.11		80	80		
3	14.2	10.3	6.0	3	250	0.7		1.58	611.6	83	78		
4	19.9	10.0	6.4	6	271	0.7		1.08	3.6	85	78		
5	25.6	9.8	6.4	9	278	0.7		1.08	5.4	86	79		
6	31.3	11.3	5.8	12	285	0.7		1.06	7.2	87	80		
AVERAGE		-0.1	-0.1	15	288	1.0		1.37	8.9	88	81		
PITOT LEAK CHECK:	SPAN	-0.1	0.0					FINAL	620.825				

BEFORE: TOP ΔP = 2.8

AFTER: TOP ΔP = 1.4

BEFORE: BOTTOM ΔP = 2.2

AFTER: BOTTOM ΔP = 0.8

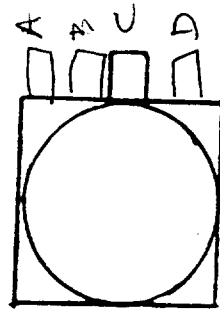
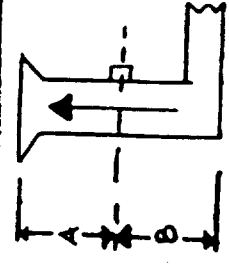
BEFORE: SAMPLE TRAIN LEAK: CFM @ 15 IN. HG.

AFTER: CFM @ 15 IN. HG.

COMMENTS: PURGE

Production rate 217 tons/hour.

PLANT: Grain Elevator
LOCATION: Burlington
COUNTY: _____
UNIT: _____
DATE: 5/8/90
RUN NO./METHOD: 2 (continued)
COLD BOX NO.: 2
METER BOX NO.: B
METER FACTOR: _____
PITOT #/ FACTOR: _____
PYROMETER #: _____
MAGNETIC FACTOR: ΔP _____ ΔH _____



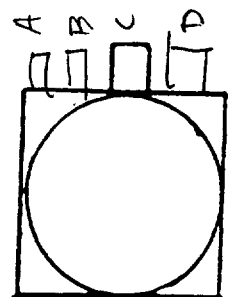
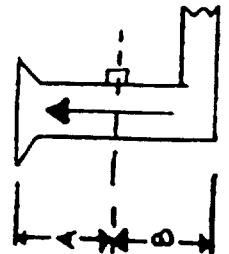
FILTER NO.: C-17
AMBIENT TEMP.: 81
BAROMETRIC PRESS., IN. HG.: 29.74
ASSUMED MOISTURE: _____
HEATER BOX SETTING: _____
PROBE LENGTH, FT.: _____
NOZZLE DIAMETER, IN.: #24, 0.235
PROBE HEATER SETTING: _____
APPROX. WIND VEL., MPH: _____
SAMPLE BOX TEMP., (F): 230 F
STATIC PRESSURE: _____
OFFSET: _____ in. PORT DIA.: _____ in. (M / F)

TRAVERSE POINT NUMBER	DISTANCE INCHES	O2 (%)	CO2 (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY IN. H2O		PRESSURE DIFF ORIFICE METER (ΔH)	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GAS METER		PUMP VACUUM IN. HG	TEMP. LAST IMPINGER (F)
						ΔP	ΔP			INLET (Tm),	OUTLET (Tm)		
1	2.8	6.8	4.8	0	27	0.3		0.50	620.825	85	84	5	
2	8.5	11.3	5.2	3	231	0.4		0.67	2.0	88	83		
3	14.2	10.3	6.0	6	280	0.5		0.84		91	84		
4	19.9	9.8	6.2	9	280	0.7		1.08	25.0	91	85	7	
5	25.6	10	6.2	12	281	0.8		1.23	6.5	92	85	8	
6	31.3	11	5.8	15	280	0.8		1.23	8.4	94	86		
AVERAGE		10.9	5.5	72	267.2		0.866	FINAL 1.028	644.731	84.1			

PITOT LEAK CHECK: BEFORE: TOP ΔP= _____ ΔP= _____ AFTER: TOP ΔP= _____ ΔP= _____
SAMPLE TRAIN LEAK: BEFORE= _____ CFM@ _____ IN. HG. AFTER= _____ CFM@ _____ IN. HG.
COMMENTS: _____ PURGE _____

Nov 21 1998

PLANT: Garfield
 LOCATION: Duettan
 COUNTY: Santa Barbara
 UNIT: #6
 DATE: 5/8/90
 RUN NO. METHOD: 3 PART
 COOLD BOX NO.: #6
 METER BOX NO.: D
 METER FACTOR: 1.0
 PITOT #/ FACTOR: 1.0
 PYROMETER #: 1.1
 MAGNEHELIC FACTOR: ΔP ΔH



FILTER NO. C-18
 AMBIENT TEMP.: 74
 BARMETRIC PRESS., IN. HG.: 29.7
 ASSUMED MOISTURE: 28%
 HEATER BOX SETTING: Hi
 PROBE LENGTH, FT.: 5'
 NOZZLE DIAMETER, IN.: #22 0.226" dia
 PROBE HEATER SETTING: Hi
 APPROX. WIND VEL., MPH: 0
 SAMPLE BOX TEMP., (F): 225
 STATIC PRESSURE: -0.4 "H₂O P_{static} = 29.7
 OFFSET: in. PORT DIA.: in. (M / F)

TRAVERSE POINT NUMBER	DISTANCE INCHES	O2 (%)	CO2 (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY IN. H2O		PRESSURE DIFF ORIFICE METER (ΔH) IN. H2O	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GAS METER		PUMP VACUUM IN. HG	TEMP. LAST IMPINGER (F)
						ΔP	ΔP			INLET (Tm),	OUTLET (TM)		
D-1	2.0	13.3	4.2	12:15	240	1.4		1.98	645.088	83	83	13	
2	8.5	11.0	5.2	3	250	1.3		1.84	7.5	83	83		
3	14.2	12.0	4.4	6	254	0.9		1.27	50.0	85	83		
4	19.7	11	5.3	9	258	0.9		1.25	52.0	87	82		
5	25.6	12	4.9	12	258	0.7		.98		87	83		
6	31.3	11.8	5.9	15	243	0.7		.98	5.3	90	83		
B-1	2.8	15.5	2.7					FINAL	657.039				
2	8.5	11.3	5.2	0	265	0.4		0.56		87	87		
3	14.2	10.3	5.8	3	256	0.4		0.56	8.2	91	86		
4	19.9	16.0	5.8	6	265	0.4		0.56	9.7	92	86		
5	25.6	10.0	5.9	9	268	0.6		0.83	60.9	93	87		
6	31.3	9.9	6.1	12	273	0.8		1.11	2.3	95	87	8	
AVERAGE				15	277	1.0		1.53	4.1	99.6	89	10	
								FINAL	666.107				

PITOT LEAK CHECK:

BEFORE: TOP ΔP = 1.0
 ΔP = 1.0
 AFTER: TOP ΔP = 3.0
 ΔP = 3.0

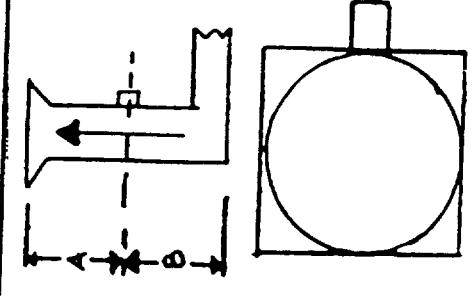
BOTTOM ΔP = 3.2
 ΔP = 3.2
 BOTTOM ΔP = 2.7
 ΔP = 2.7

BEFORE: 0.02 IN. HG.
 AFTER: 0.02 IN. HG.
 COMMENTS: 26 DEC 03 to 033

PURGE

Production Rate, run #3 = 222 Tons/hour.

PLANT: Granite
 LOCATION: Pineville
 COUNTY: Santa Barbara
 UNIT: _____
 DATE: 5/8/90
 RUN NO./METHOD: 2 Part
 COLD BOX NO.: #6
 METER BOX NO.: _____
 METER FACTOR: _____
 PITOT #/ FACTOR: _____
 PYROMETER #: _____
 MAGNEHELIC FACTOR: ΔP _____ ΔH _____



FILTER NO.: C-18
 AMBIENT TEMP.: 74
 BARAMETRIC PRESS., IN. HG.: 29.7
 ASSUMED MOISTURE: 28%
 HEATER BOX SETTING: _____
 PROBE LENGTH, FT.: _____
 NOZZLE DIAMETER, IN.: .226
 PROBE HEATER SETTING: _____
 APPROX. WIND VEL., MPH: 0
 SAMPLE BOX TEMP., (F): 72.5
 STATIC PRESSURE: -.4 "H₂O
 OFFSET: _____ in. PORT DIA.: _____ in. (M / F)

TRAVERSE POINT NUMBER	DISTANCE INCHES	O ₂ (%)	CO ₂ (%)	SAMPLE TIME MIN.	STACK TEMP. (Ts), F	VELOCITY IN. H ₂ O		PRESSURE DIFF ORIFICE METER (ΔH)	DRY GAS SAMPLE VOLUME (VM), FT.	GAS SAMPLE TEMP. @ DRY GAS METER		PUMP VACUUM IN. HG.	TEMP. LAST IMPINGER (F)
						ΔP	ΔP			INLET (Tm)	OUTLET (Tm)		
C-1	2.8	10.0	6.0	0	269	0.5		0.70	666.107	92	92		
2	8.5	9.8	5.8	3	284	0.6		0.82	7.5	95	91		
3	14.2	10.3	5.6	6	286	0.6		0.82	9.1	96	90		
4	19.9	10.3	4.0	9	279	0.6		0.82	70.5	97	92		
5	25.6	10.0	5.9	12	279	0.6		0.82	2.6	98	92		
6	31.3	11.3	5.2	15	279	0.7		1.23	4.0	99	92		
A-1	1.8	11.0	5.2	1:21	270	0.1		FINAL	675.929				
2	8.5	10.3	6.0	3	247	0.4		0.14		96	95		
3	14.2	10.3	5.8	6	270	0.5		0.57	6.5	96	94		
4	19.9	10.0	5.9	9	274	0.6		0.72	7.7	98	94		
5	25.6	—	—	12	277	0.8		0.87	9.1	98	93		
6	31.3	—	—	15	281	0.8		1.11	680.6	99	93		
AVERAGE		10.15	5.2					1.19		100	94		
								FINAL	684.267	96.9	94		
PITOT LEAK CHECK: 11.1 5.2 12 266A 0.815 BEFORE: TOP ΔP= _____ BOTTOM ΔP= _____ AFTER: TOP ΔP= _____ BOTTOM ΔP= _____ SAMPLE TRAIN LEAK: _____ IN. HG. _____ IN. HG.													
COMMENTS: _____ PURGE _____													

VIII. QUALITY ASSURANCE

DRY GAS METER CALIBRATION

Date: 5/5/90

Unit: B

Ambient Conditions

Temp: 83 F/C

Baro: 29.85 in.Hg

ORIFICE MANOMETER SETTING D,H	GAS VOL WET TEST METER V,w	GAS VOL DRY GAS METER Vb,	wet test tw	Temperature				Y	DH@Y
				Dry IN	Dry Out	Ave f	Time e min		
				TD, IN	Tdo,	Td,			
0.5	5	544.909	77	86	84	87.25	13.22	0.9400	1.9597
		539.500	78	94	85				
1.0	5	550.614	78	91	87	91.00	9.58	0.9435	2.0479
		545.200	78	98	88				
1.5	5	556.543	78	91	90	92.75	7.83	0.9403	2.0456
		551.100	78	100	90				
2.0	5	562.356	78	96	91	95.00	6.8	0.9407	2.0488
		556.900	78	102	91				
								0.941	2.026

Calibration by: RTR

Meter Factor: 0.9411

Reviewed by: _____

Delta H: 2.0255

Equations:

$$Y = (V_w \cdot P_b) \cdot (T_d + 460) / (V_d \cdot T - V_{db} \cdot T) + (D_e \cdot H / 13.6) \cdot (((W_t + w_t) / 2) + 460)$$

$$D_e \cdot H = (0.0317 \cdot D_e) \cdot (((((W_t + W_t) / 2) + 460) \cdot e) / V_w)^2 / ((P_b \cdot (T_d + 460))$$

PITOT TUBE CALIBRATION RECORD

Date: 7/1/89

Unit: #7-5'

Ambient Condition

Temp: 76 F/C

Baro: 30.07 in. Hg

Run No.	AP In.H2O Standard	AP IN. H2O Type"S"		Cp (S)	
		A	B	A	B
1	0.27	0.39	0.38	0.8237	0.8345
2	0.62	0.88	0.89	0.8310	0.8263
3	0.95	1.34	1.35	0.8336	0.8305
Average =				0.8294	0.8304
Average Both Side =				0.8299	

Calibrated by: RTR

Reviewed by: CDD

Cp(a)-Cp(b)= 0.001

Sa	Sb
0.005	0.004

PITOT TUBE CALIBRATION RECORD

Date: 7/5/89

Unit: #2-5'

Ambient Condition

Temp: 83 F/C

Baro: 30.04 in. Hg

Run No.	AP In.H2O Standard	AP IN. H2O Type "S"		Cp (S)	
		A	B	A	B
1	0.25	0.34	0.33	0.8489	0.8617
2	0.49	0.68	0.69	0.8404	0.8343
3	0.93	1.31	1.3	0.8341	0.8373
Average =				0.8411	0.8444
Average Both Side =				0.8428	

Calibrated by: RTR
Reviewed by: CDD

Cp(a)-Cp(b)= 0.003

Sa	Sb
0.007	0.015

THERMO COUPLE CALIBRATION

Date: 1/15/90

Unit: T-1

Point	* Standard Temperature <i>Tstd</i>		Pyrometer Temperature <i>Tpyr</i>		Error % ** $(Tstd - Tpyr)/Tstd$
	deg. F		deg. F		
1 Ambient	62.5		59.0		0.67%
2 Ice	33.0		31.4		0.32%
3 Boil	213.0		213.0		0.00%
4 Oil					#VALUE!

Std. Corr. Factor

1.037

Calibration by: RTR

* Standard ID: Labcraft-#227-694

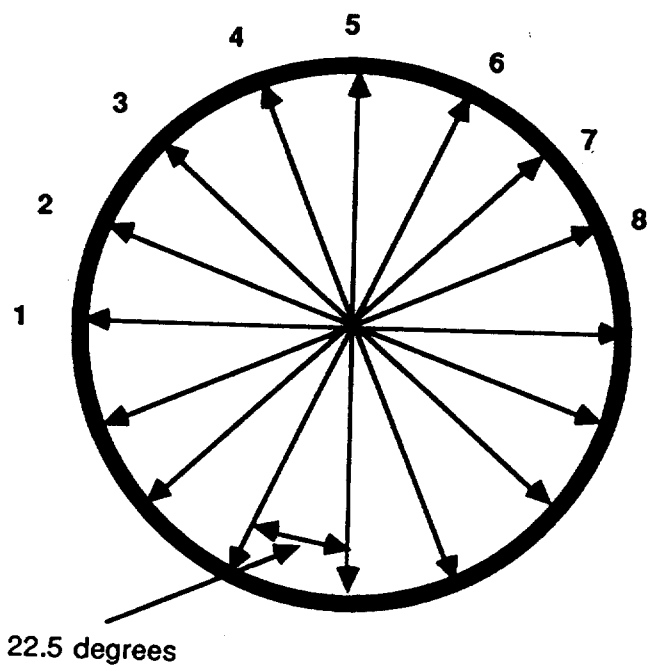
Reviewed by:

** in deg. K

Nozzle Calibration

Nozzle I.D. : #24

Date : 01/08/90



Points

- | | |
|----|--------------|
| 1- | <u>0.234</u> |
| 2- | <u>0.233</u> |
| 3- | <u>0.235</u> |
| 4- | <u>0.235</u> |
| 5- | <u>0.237</u> |
| 6- | <u>0.238</u> |
| 7- | <u>0.236</u> |
| 8- | <u>0.235</u> |

Average Nozzle Diameter = 0.235

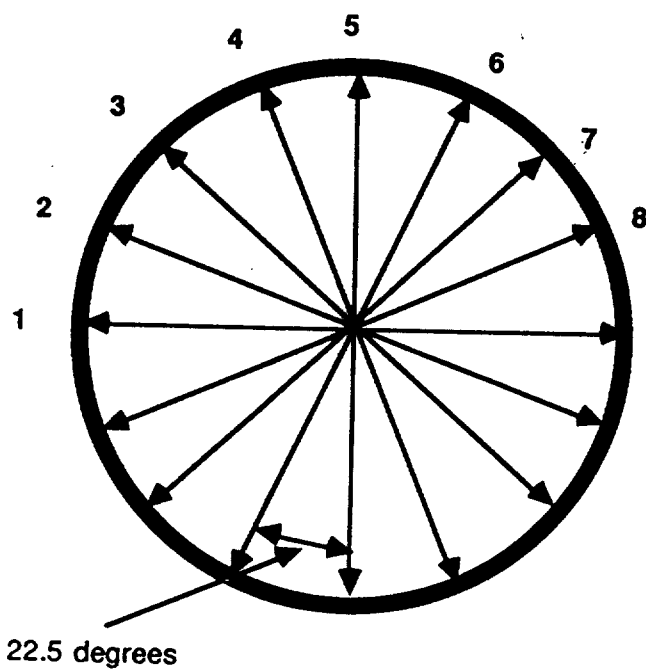
Analyst : RTB

Reviewed :

Nozzle Calibration

Nozzle I.D. : 22

Date : 1/8/90



Points

- 1- 0.227
- 2- 0.226
- 3- 0.225
- 4- 0.225
- 5- 0.225
- 6- 0.225
- 7- 0.226
- 8- 0.226

Average Nozzle Diameter = 0.226

Analyst : RTB

Reviewed :

BTC Environmental, Inc. - 1989

MAGNEHELIC CALIBRATION

DATE: 2/28/90
 GAGE ID # M-3
 RANGE 0-5 in. H2O

SCHEDULED CALIBRATION:

SEMI ANNUAL ☒
 BI-MONTHLY ☐
 OTHER ☐

REFERENCE
 ID # 0-10 DWYER MANO

LEAK CHECK:

System:	† Set @ 10 in. H2O	vacuum 10 in. P F	pressure 10 in. P F
Point:	†† Set @ 90 % FS in. H2O	vacuum in. P F	pressure in. P F

Point	Incline Delta P Pinc	Magnehelic Delta P Pmag	% Deviation (Pinc-Pmag)/Pinc x 100
1	1.000	1.02	2.000%
	1.000	1.03	3.000%
	1.000	1.02	2.000%
average	1.00	1.02	** 2.333%
2	2.000	2.05	2.500%
	2.000	2.05	2.500%
	2.000	2.05	2.500%
average	2.00	2.05	** 2.500%
3	3.000	3.05	1.667%
	3.000	3.05	1.667%
	3.000	3.05	1.667%
average	3.00	3.05	** 1.667%
4	4.000	4.05	1.250%
	4.000	4.05	1.250%
	4.000	4.05	1.250%
average	4.00	4.05	** 1.250%
5	5.000	5.05	1.000%
	5.000	5.05	1.000%
	5.000	5.05	1.000%
average	5.00	5.05	** 1.000%

STANDARD CORRECTION FACTOR

AVERAGE DEVIATION
 STANDARD DEVIATION
 95% CONFIDENCE INTERVAL
 PRECISION(within +/- 3%)

0.983
0.018
0.006
0.015
-0.97

† If pressure or vacuum decreases by more than 1 in. in 5 minutes then remove from service.
 †† If pressure or vacuum decreases by more than 5% in 5 minutes then remove from service.
 ** These values must be within +/- 5% before the magnehelic can be put into operation.

Calibration by: RTR

Reviewed by: MRP

MAGNEHELIC CALIBRATION

DATE: 2/28/90
 GAGE ID # M-4
 RANGE 0-2 in. H2O

SCHEDULED CALIBRATION:
 SEMI ANNUAL ☒
 BI-MONTHLY ☐
 OTHER ☐

REFERENCE
 ID # 0-10 DWYER MANO

LEAK CHECK:

System:	† Set @ 10 in. H2O	vacuum 10 in. P F	pressure 10 in. P F
Point:	†† Set @ 90 % FS in. H2O	vacuum in. P F	pressure in. P F

Point	Incline Delta P Pinc	Magnehelic Delta P Pmag	% Deviation (Pinc-Pmag)/Pinc x 100
1	0.400	0.43	7.500%
	0.400	0.42	5.000%
	0.400	0.43	7.500%
average	0.40	0.43	** 6.667%
2	0.800	0.83	3.750%
	0.800	0.84	5.000%
	0.800	0.83	3.750%
average	0.80	0.83	** 4.167%
3	1.200	1.25	4.167%
	1.200	1.25	4.167%
	1.200	1.25	4.167%
average	1.20	1.25	** 4.167%
4	1.600	1.64	2.500%
	1.600	1.63	1.875%
	1.600	1.63	1.875%
average	1.60	1.63	** 2.083%
5	2.000	2.05	2.500%
	2.000	2.05	2.500%
	2.000	2.05	2.500%
average	2.00	2.05	** 2.500%

STANDARD CORRECTION FACTOR

AVERAGE DEVIATION
 STANDARD DEVIATION
 95% CONFIDENCE INTERVAL
 PRECISION(within +/- 3%)

0.963
0.039
0.017
0.043
-0.92

† If pressure or vacuum decreases by more than 1 in. in 5 minutes then remove from service.
 †† If pressure or vacuum decreases by more than 5% in 5 minutes then remove from service.
 ** These values must be within +/- 5% before the magnehelic can be put into operation.

Calibration by: RTR

Reviewed by: MRP



SCOTT-MARRIN, INC.
2001 THIRD ST. • UNIT H • RIVERSIDE, CA 92507
TELEPHONE (714) 784-1240

REPORT OF ANALYSIS
NIST TRACEABLE GAS MIXTURES

BTCE01

TO:

Matthew Pena
BTC Enviromental
1536 Eastman Ave. Suite B
Ventura, CA 93003

DATE : 02/21/90

CUSTOMER ORDER NUMBER: 02685

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CYLINDER NUMBER	COMPONENT	CONCENTRATION (v/v)	NIST TRACEABLE REFERENCE STANDARD
CC28058	Oxygen	$7.57 \pm 0.08 \%$	SRM 2658a
	Carbon Monoxide	$396 \pm 4 \text{ ppm}$	SRM 1680b
	Carbon Dioxide	$11.67 \pm 0.12 \%$	SRM 1675b
	Nitrogen	Balance	
CC60289	Oxygen	$15.22 \pm 0.15 \%$	SRM 2659
	Carbon Monoxide	$400 \pm 4 \text{ ppm}$	SRM 1680b
	Carbon Dioxide	$4.25 \pm 0.04 \%$	SRM 2626a
	Nitrogen	Balance	
CC60380	Oxygen	$7.84 \pm 0.08 \%$	SRM 2658a
	Carbon Dioxide	$11.58 \pm 0.12 \%$	SRM 1675b
	Nitrogen	Balance	

ppm = umole/mole

% = mole-%

The above analyses are traceable to the National Institute of Standards and Technology by intercomparison with the reference standards listed above. Where indicated, volumetric and gravimetric reference standards are traceable thru use of our analytical balance. NIST Report No. MMAP 232.09/202491.

Analyst:

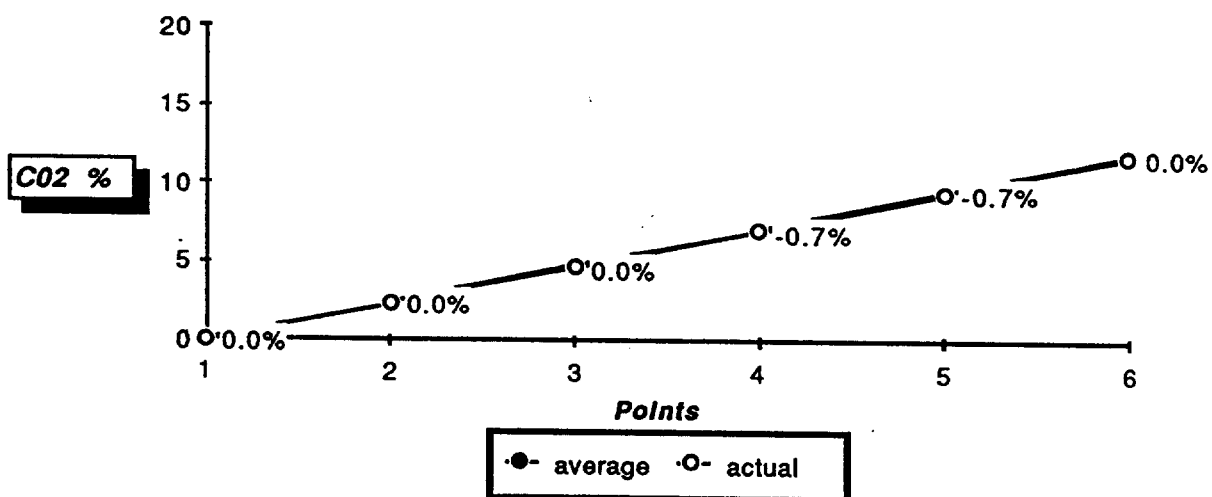
J.W. Gay

Approved:

J.T. Marrin

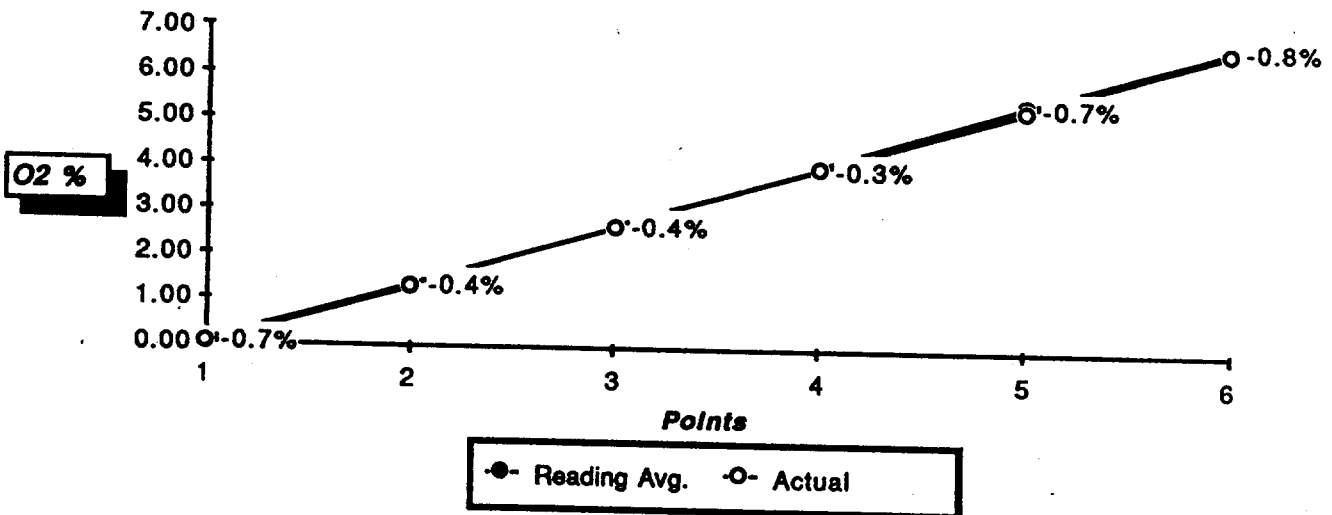
The only liability of this company for gas which fails to comply with this analysis shall be replacement or reanalysis thereof by the company without extra cost.

ACS 3300 #4 - December 5, 1990



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Teledyne 320 AX - unit #5
September 19, 1989



SULFUR DIOXIDE - ULTRAVIOLET METHOD

Instrument Manufacture: Anarad, Inc.
534 E. Ortega St.
Santa Barbara, CA 93103

Unit #1 - Model: AR-30, equipped with Model AR-50DD digital display.
Serial Number: 2564, Measurement ranges: 0-100, 1000 ppmv SO₂.

Instrument Manufacture: Western Research
#122-1300 South Potomac St.
Aurora, Colorado 80012

Unit #2 - Model: 721AT2
Serial Number: 89-721AT2-7567-1, Measurement ranges: 0-200, 0-2000

CARBON DIOXIDE - NON-DISPERSIVE INFRARED METHOD (2 units)

Instrument Manufacture: Horiba Instruments, Inc.
1021 Duryea Avenue
Irvine, CA 92714

Unit #1 - Model: MEXA-221
Serial Number: 4726203, Measurement range: 0-5, 20% CO₂

Unit #2 - Model: MEXA-211E
Serial Number: E70019, Measurement range: 0-5, 20% CO₂

Instrument Manufacture: Automated Custom Systems inc.
1238 West Grove Avenue
Orange, Ca. 92665-4134

Unit #3 - Model: ACS 3300 NDIR
Serial Number: N8M6611T, Measurement range: 0-5, 20% CO₂

Unit #4 - Model: ACS 3300 NDIR
Serial Number: N9c5479T, Measurement range: 0-5, 20% CO₂

OXYGEN-PARAMAGNETIC SUSCEPTIBILITY METHOD (3 units)

Instrument Manufacture: Taylor Instrument Company
95 Omnes Street
Rochester, NY 14601

Unit #1 - Model: Servomex OA580
Serial number: 580/702/497, Measurement range: 0-10, 25, 100% O₂.

Unit #2 - Model: Servomex 570A
Serial number: 68771/B, Measurement range: 0-100% O₂.

Unit #3 - Model: Servomex 570A
Serial number: 4212B, Measurement range: 0-100% O₂.

OXYGEN-ELECTROCHEMICAL METHOD (2units)

Instrument Manufacture: Teledyne Analytical Instruments
16830 Chestnut St.
City of Industry, CA. 91749-1580

Unit #4 - Model: Teledyne 320AX
Serial number: 107294, Measurement range: 0-5, 10, 25% O₂

Unit #4 - Model: Teledyne 320AX
Serial number: 108743, Measurement range: 0-5, 10, 25% O₂

CHAIN OF CUSTODY RECORD

[illegible]