

AP42 Section: 11.1

Reference Number: 55

Title: Results Of The September 8, 1993 Particulate And Visual Emission Compliance Test On The Baghouse Outlet At The Commercial Asphalt Company Facility Located In Ramsey, Minnesota,

Pace, Inc., Golden Valley, MN,

September 21, 1993.

1394T

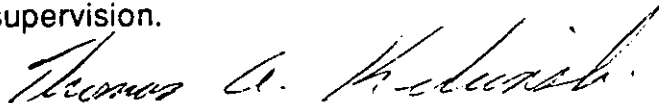
RESULTS OF THE SEPTEMBER 8, 1993
PARTICULATE AND VISUAL EMISSION
COMPLIANCE TEST ON THE BAGHOUSE
OUTLET AT THE COMMERCIAL ASPHALT
COMPANY FACILITY LOCATED IN
RAMSEY, MINNESOTA

Prepared For: Mr. Brent Schlueter
Commercial Asphalt Company

Prepared By: PACE, Incorporated
1710 Douglas Drive North
Golden Valley, Minnesota 55422

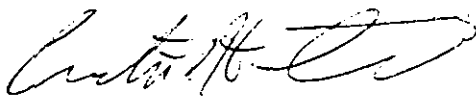
PACE Project No.: 930831.402
Report Date: September 21, 1993

Field sampling was performed by me and personnel under my direct supervision.



Thomas A. Kuchinski
Project Field Supervisor

All sampling, analysis and data reduction were performed by PACE,
Incorporated under my supervision.



Curtis H. Stock
Supervisor, Air Sampling Section

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EXECUTIVE SUMMARY

PACE Incorporated was contracted by Commercial Asphalt Company to perform particulate and visual emissions testing on the Baghouse Outlet at the Commercial Asphalt Company facility located in Ramsey, Minnesota. This series of tests was performed on September 8, 1993. The results are summarized with pertinent process data in the following table:

Test Results Summary

	<u>Run 1</u>	<u>Run 3</u>	<u>Run 4</u>	<u>Average</u>
Stack Temperature	222	241	242	235
Moist Content Flue Gas	34.3	33.6	34.9	34.3
Airflows				
ACFM	86600	82800	82200	84200
DSFM	42900	40300	39800	41000
Particulate Concentration				
GR/DSCF Dry Catch	0.018	0.016	0.016	0.017
GR/DSCF Dry & Wet Catch	0.021	0.020	0.019	0.020
Particulate Emission Rate				
LB/HR	7.7	6.9	6.4	7.0
Opacity %	0			
Aggregate Mix Moisture %	3.0	5.1	5.6	4.6
Plant Reduction Rate				
TPH	592.5	575.8	571.8	580.0

INTRODUCTION

PACE, Incorporated personnel conducted particulate and visual emission compliance testing on the Baghouse Outlet at the Commercial Asphalt Company located in Ramsey, Minnesota. On-site testing was performed by a three member team consisting of T. Kuchinski, M. Loftus and M. Wilson. Coordination between plant operations and testing activities was provided by Tyler Nelson and Mike Mahoney of Commercial Asphalt Company through direct contact with the test team leader. Testing was not witnessed by a representative of the Minnesota Pollution Control Agency. The test consisted of three independent one-hour samplings for particulate with concurrent integrated gas sampling for Orsat analyses. Aggregate and fuel samples were collected during each run and visible emissions were evaluated by a certified observer.

The objectives of this project were to quantify particulate emissions and compare them to applicable air emissions regulations stipulated by Minnesota Rules. Special provisions for this test program include operating at maximum capacity and firing with waste oil.

Results are summarized in the next section followed by descriptions of the process under investigation and test methods. All supporting data are included in subsequent appendices.

RESULTS SUMMARY

Results of particulate determinations and gas composition are summarized in Table 1. The particulate emission rate averaged 7.0 LB/HR at an average particulate concentration of .017 GR/DSCF Dry Catch and .020 GR/DSCF Dry & Wet Catch. Minnesota Pollution Control Agency emissions regulations limit sources of this type to 0.04 GR/DSCF.

Opacity observations were recorded every 15 seconds for a one-hour period during the first run. These results are shown in Table 4. All of the 240 observations are zero percent. Within the one-hour observation period, the highest average opacity for a consecutive six-minute time span was zero percent. The average opacity for the one-hour period was zero percent.

During Run 2, problems were encountered with the firing unit to the drum dryer and testing had to be stopped. Run 2 was terminated and a fourth run was conducted. On this and after complete review of the test results, we believe that the values reported herein are an accurate representation of the source conditions at the time of the test.

Commercial Asphalt Company
 Ramsey, Minnesota
 PACE Project No. 930831.401

PACE Incorporated
 September 15, 1993

TABLE 1
SUMMARY OF THE RESULTS
TEST 1

Baghouse Outlet

Parameter	Run 1	Run 3	Run 4	Average
Date of Run	9/8/93	9/8/93	9/8/93	
Time of Run	715-824	1251-1402	1501-1610	
Asphalt Production TPH	592.5	575.8	571.8	580.0
Recycle Usage (Percent)	37.0	29.4	29.5	32.0
Fuel Input (GPH)	780.0	760.0	780.0	773.3
Volumetric Flow Rate				
ACFM	86600	82800	83200	84200
DSCFM	42900	40300	39800	41000
Gas Temperature (°F)	222	241	242	235
Gas Moisture Content (%v/v)	34.3	33.6	34.9	34.3
Gas Composition (%v/v, Dry)				
CO2	6.5	7.8	7.7	7.3
O2	12.4	10.8	10.7	11.3
N2	81.1	81.5	81.6	81.4
Isokinetic Variation (%)	100.5	97.6	101.7	
Particulate Emission Rate (LB/HR)	7.7	6.9	6.4	7.0
Particulate Concentration				
GR/ACF, Total	0.010	0.010	0.009	0.010
GR/DSCF, Total	0.021	0.020	0.019	0.020
GR/DSCF, Dry Catch Only	0.018	0.016	0.016	0.017

RESULTS OF ORSAT AND MOISTURE DETERMINATIONS

Commercial Asphalt Company
 Ramsey, Minnesota
 PACE Project No. 930831.401

PACE Incorporated
 September 15, 1993

TABLE 2
RESULTS OF ORSAT AND MOISTURE DETERMINATIONS
TEST 1

Baghouse Outlet

Parameter	Run 1	Run 3	Run 4
Date of Run	9/8/93	9/8/93	9/8/93
Time of Run	715-824	1251-1402	1501-1610
ORSAT (%v/v)			
Dry Basis			
Carbon Dioxide	6.50	7.75	7.70
Oxygen	12.40	10.80	10.70
Carbon Monoxide*	*	*	*
Nitrogen	81.10	81.45	81.60
WetBasis			
Carbon Dioxide	4.27	5.15	5.02
Oxygen	8.15	7.17	6.97
Carbon Monoxide*	*	*	*
Nitrogen	53.28	54.09	53.15
Portable Oxygen Monitor Result			
Time Weighted Average (%O2)	**	**	**
Moisture Collected (ml)	520.0	460.0	500.0
Moisture Content (%v/v)	34.30	33.59	34.86
Molecular Weight of Flue Gas (lb/lb-mole)			
Dry	29.54	29.67	29.66
Wet	25.58	25.75	25.60
Fo	1.308	1.303	1.325

*Carbon monoxide was not measured, assumed concentrations less than 0.01%.

* **Did not use Portable Oxygen Analyzer because it was not working correctly.

RESULTS OF PARTICULATE LOADING DETERMINATIONS

Commercial Asphalt Company
Ramsey, Minnesota
PACE Project No. 930831.401

PACE Incorporated
September 15, 1993

TABLE 3
RESULTS OF PARTICULATE LOADING DETERMINATIONS
TEST 1

Baghouse Outlet

Parameter	Run 1	Run 3	Run 4
Date of Run	9/8/93	9/8/93	9/8/93
Time of Run	715-824	1251-1402	1501-1610
Sample Duration (Min.)	60.0	60.0	60.0
Average Flue Gas Temperature (°F)	222.4	241.4	242.3
Moisture Content of Flue Gas (%v/v)	34.30	33.59	34.86
Particulate Collected (Mg)			
Wet Catch	7.3	10.7	9.0
Dry Catch	56.1	44.7	44.8
Total	63.4	55.4	53.8
Volumetric Flow Rate			
ACFM	86590	82760	83250
SCFM	65340	60750	61030
DSCFM	42920	40350	39760
Sample Volume (Cubic Feet)			
Meter Conditions	48.19	45.90	47.06
Dry Standard	46.88	42.81	43.98
Isokinetic Variation (%)	100.5	97.6	101.7
Particulate Concentration			
Wet Catch, GR/DSCF	0.002	0.004	0.003
Dry Catch, GR/DSCF	0.018	0.016	0.016
Total, GR/DSCF	0.021	0.020	0.019
Particulate Emission Rate*			
Total, LB/HR	7.67	6.91	6.44

*Dry catch plus organic/residual wet catch

Commercial Asphalt Company
 Ramsey, Minnesota
 PACE Project No. 930831.401

PACE Incorporated
 September 15, 1993

TABLE 4
RESULTS OF OPACITY OBSERVATIONS
TEST 1

Baghouse Outlet

<u>Percent Opacity</u>	<u>Optical Density</u>	<u>Relative Frequency</u>
0	0.000	100.00
5	0.022	0.00
10	0.046	0.00
15	0.071	0.00
20	0.097	0.00
25	0.125	0.00
30	0.155	0.00
35	0.187	0.00
40	0.222	0.00
45	0.260	0.00
50	0.301	0.00
55	0.347	0.00
60	0.398	0.00
65	0.456	0.00
70	0.523	0.00
75	0.602	0.00
80	0.699	0.00
85	0.824	0.00
90	1.000	0.00
95	1.301	0.00
99	2.000	0.00

Average > 0.0

0.000

Total > 100

Average Opacity Per Six Minute Period:

Period	Opacity	Period	Opacity
1	0.0	6	0.0
2	0.0	7	0.0
3	0.0	8	0.0
4	0.0	9	0.0
5	0.0	10	0.0

High Six Minute Average: 0.0

Maximum reading: 0.0

Minumum reading: 0.0

Observer: M. Loftus

Date of test: 9/8/93

Time of test: 715-815

NOTE: The high six minute average opacity might not coincide with any of the 10 reported six minute periods. The high value is the maximum consecutive period possible and may overlap two of the ten consecutive six-minute periods.

November 5, 1993

Mr. Brent Schlueter
Commercial Asphalt Company
P.O. Box 1480
10633 89th Avenue North
Maple Grove, MN 55311-6480

RE: PACE Project No. 930831.402
Fuel Analysis Report

Dear Mr. Schlueter,

At the request of PACE, Inc., Minnesota Valley Testing Laboratories is currently conducting a second Total Halogen analysis on the fuel samples collected on September 8, 1993 at the Hox Mix Asphalt Plant located in Ramsey, Minnesota. This analysis is to verify the results analyzed on October 10, 1993.

The results should be provided to me by November 11, 1993.

I'm sorry for the delay and hope this causes no inconveniences for you.

If you have any questions or comments, please feel free to contact me at (612) 525-3364.

Respectfully,



Michael Loftus
Project Manager, Air Sampling Department

CHS/cjn

Enclosures

November 16, 1993

Mr. Brent Schlueter
Commercial Asphalt Company
P.O. Box 1480
10633 89th Avenue North
Maple Grove, MN 55311-6480

RE: PACE Project No. 930831.402
Fuel Analysis Report

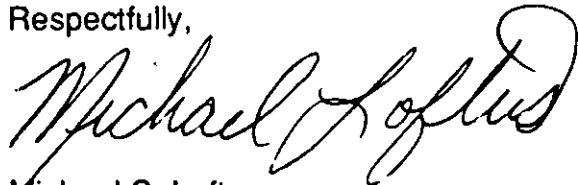
Dear Mr. Schlueter,

Please find enclosed four copies of our fuel analysis report the September 8, 1993 Particulate and Visual Emission Compliance Test on the Baghouse Outlet at the Commercial Asphalt Company Facility Located in Ramsey, Minnesota."

A duplicate analysis was performed on the Halogen content along with a Volatile Organic Compound summary.

If you have any questions or comments, please feel free to contact me or our Client Services Department at (612) 525-3364.

Respectfully,



Michael S. Loftus
Project Manager, Air Sampling Department

Commercial Asphalt, Co.
Ramsey Hot Mix Facility
Ramsey, Minnesota
930831.401

PACE Incorporated
November 16, 1993

TABLE 5
RESULTS OF FUEL ANALYSIS
TEST 1

Baghouse Stack

Analyte:	RUN 1	RUN 3	RUN 4	Average
pH	6.6	6.6	6.5	6.6
Lead (mg/kg)	44.8	53.7	54.5	51.0
PCB (ppm)	<1	<1	<1	<1
Sulfated Ash (wt. %)	0.40	0.35	0.39	0.38
Ash (wt. %)	0.90	0.84	0.81	0.85
Calorific Value (cal/g)	8070	10291	10420	9594
Calorific Value (BTU/lb)	14526	18524	18756	17269
Total Sulfur (wt. %)	0.26	0.41	0.51	0.39
Flash Point (°F)	221	225	248	231
Total Halogens (ug/g):				
Analysis on 10/27/93	1120	987	965	1024
Analysis on 11/15/93	870	1043	835	916

RESULTS OF PRELIMINARY SOURCE DETERMINATIONS

Commercial Asfalt Company
Ramsey, Minnesota
PACE Project No.

PACE Incorporated
September 1, 1993

TABLE 6
RESULTS OF AIR FLOW DETERMINATIONS
TEST 1

Baghouse Outlet

Date of Run	9/1/93
Time of Measurement	1216
Number of Sampling Ports	5
Number of Points Sampled	20
Barometric Pressure (In. Hg)	29.50
Static Pressure (In. WC)	0.33
Absolute Flue Gas Pressure (In. Hg)	29.52
Average Flue Gas Temperature (F)	204
Average Moisture Content (%v/v)	36
Flue Gas Average Velocity (Feet/Second)	40.35
Duct Dimension (Inches)	69.5x52
Duct Cross-sectional Area (Square Feet)	25.10
Volumetric Flow Rate	
ACFM	60760
SCFM	47680
DSCFM	30510

PROCESS DESCRIPTION

The Commercial Asphalt Company facility located in Ramsey, Minnesota uses a Drum Mix Hauck Furnace capable of producing asphalt paving material. It fires waste oil or natural gas as dryer fuel. The burner rating, at a setting of 100 percent, is 175 MMBTU/HR. Pollution control is facilitated by a CMI SVM-12 Baghouse which was last serviced on August 30, 1993 by having a blacklight inspection and changing the filter dust blower. The normal pressure drop across the control equipment is 5.2 inches of water. A relational flow diagram is represented by Figure 1.

For this series of tests, the average asphalt production rate was 580 TPH while burning waste oil as dryer fuel at an average rate of 773.3 GPH. The Aggregate mix moisture content averaged 4.6 percent and recycled asphalt averaged 32 percent over the three runs. The baghouse was operated at an average of 5.3 inches of water pressure drop and the average operating temperature of the drum mixer was 269°F.

Commercial Asphalt Company
Ramsey, Minnesota
Asphalt Plant Flow Diagram

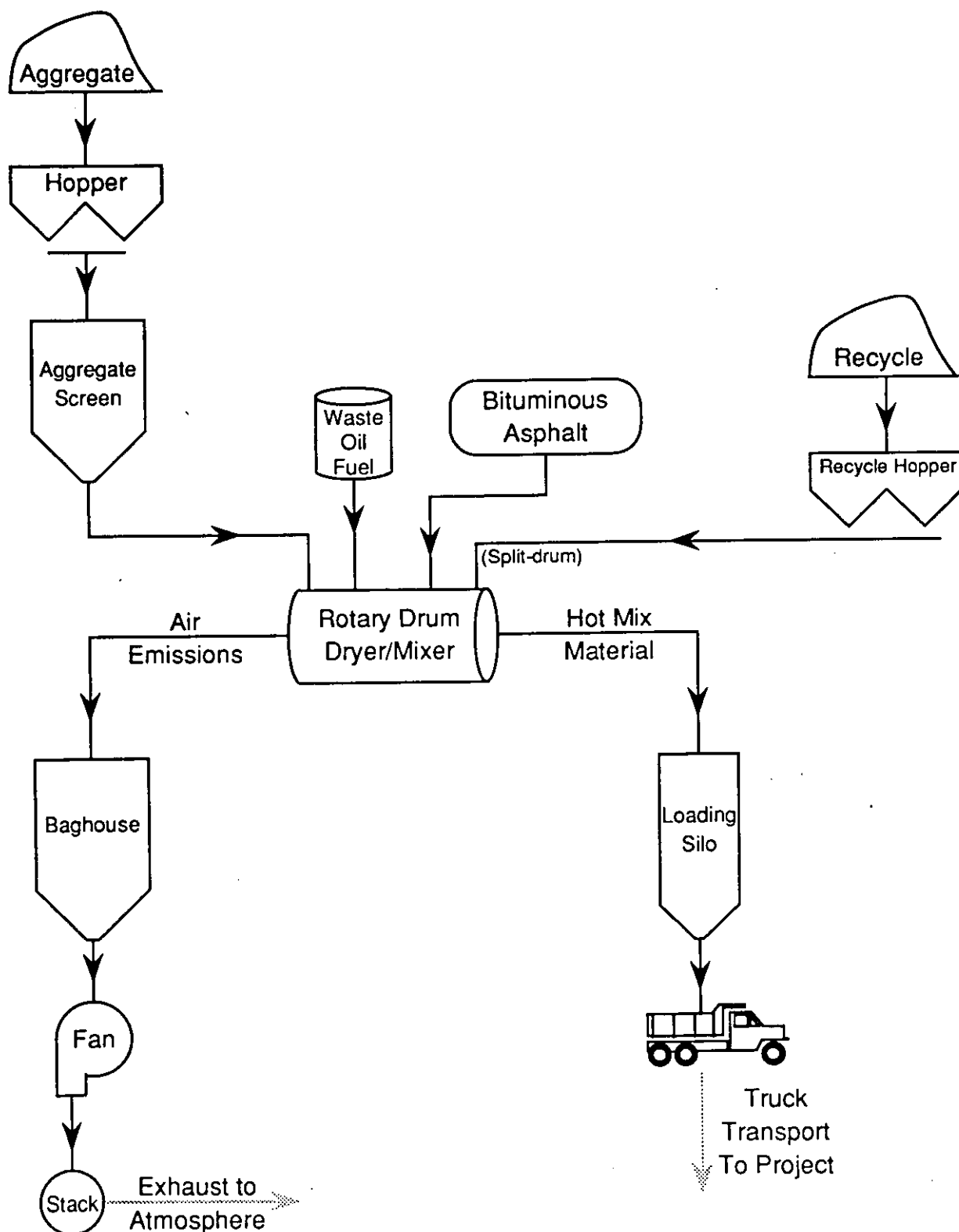


Figure 1

TEST PROCEDURES SUMMARY

Testing on the Baghouse Outlet was performed from five test ports oriented horizontally on a vertical stack, approximately 5.1 duct diameters downstream of the nearest flow disturbance and 1.3 duct diameters upstream of the stack outlet. The duct dimension at this point was verified on-site and measures 69.5" x 52". A 20 point traverse was used to extract representative flue gas samples. Each point was sampled 3 minutes for a run duration of 60 minutes. Test port and traverse point locations are displayed in Figures 2 and 3.

Particulate testing was performed in accordance with EPA Methods 1 - 5, 40 CFR 60, Appendix A. A preliminary velocity traverse and moisture estimation were conducted so that an appropriate sampling nozzle required for isokinetic sample withdrawal could be selected. A PACE sampling train that meets or exceeds the specifications outlined in the above reference was used to collect particulate samples. A temperature controlled glass-lined sampling probe was used to extract flue gas samples and transport them to an all glass filter and cyclone assembly in a temperature controlled oven. The back half of the particulate sampling train consisted of a series of three glass impingers, each of the first two prepared with 100 mls of deionized water, followed by a desiccant packed drying column. In addition, integrated gas samples were collected concurrently with the three particulate runs so that gas composition (Orsat) could be determined. Gas samples were verified in the field with a portable oxygen analyzer to ensure that no leakage occurred between the site and the laboratory. The portable oxygen analyzer was also used to monitor the oxygen content of the flue gas throughout the test.

Opacity evaluations were performed in accordance with EPA Method 9, 40 CFR 60, Appendix A. After positioning himself with respect to the sun, the source and plume (wind) direction, the certified observer proceeds to record opacity readings at 15 second intervals for one hour. A total of 240 observations is recorded in 60 minutes. The readings are integrated to calculate a one-hour average opacity and ten successive six-minute averages. In addition, computer spreadsheets are used to search the data set to find a group of 24 consecutive

readings anywhere within the one-hour evaluation for the highest possible six-minute average.

Air flow determinations were performed in accordance with EPA Method 2 using traverse point protocols specified by EPA Method 1, 40 CFR 60, Appendix A. Point velocity measurements were conducted using a S-Type pitot tube and a Neotronics Model EDM-1 Electronic Digital Manometer. Source gas moisture content was estimated using wet bulb/dry bulb temperature measurements.

Commercial Asphalt Company
Ramsey, Minnesota
Drum Dryer Baghouse Stack

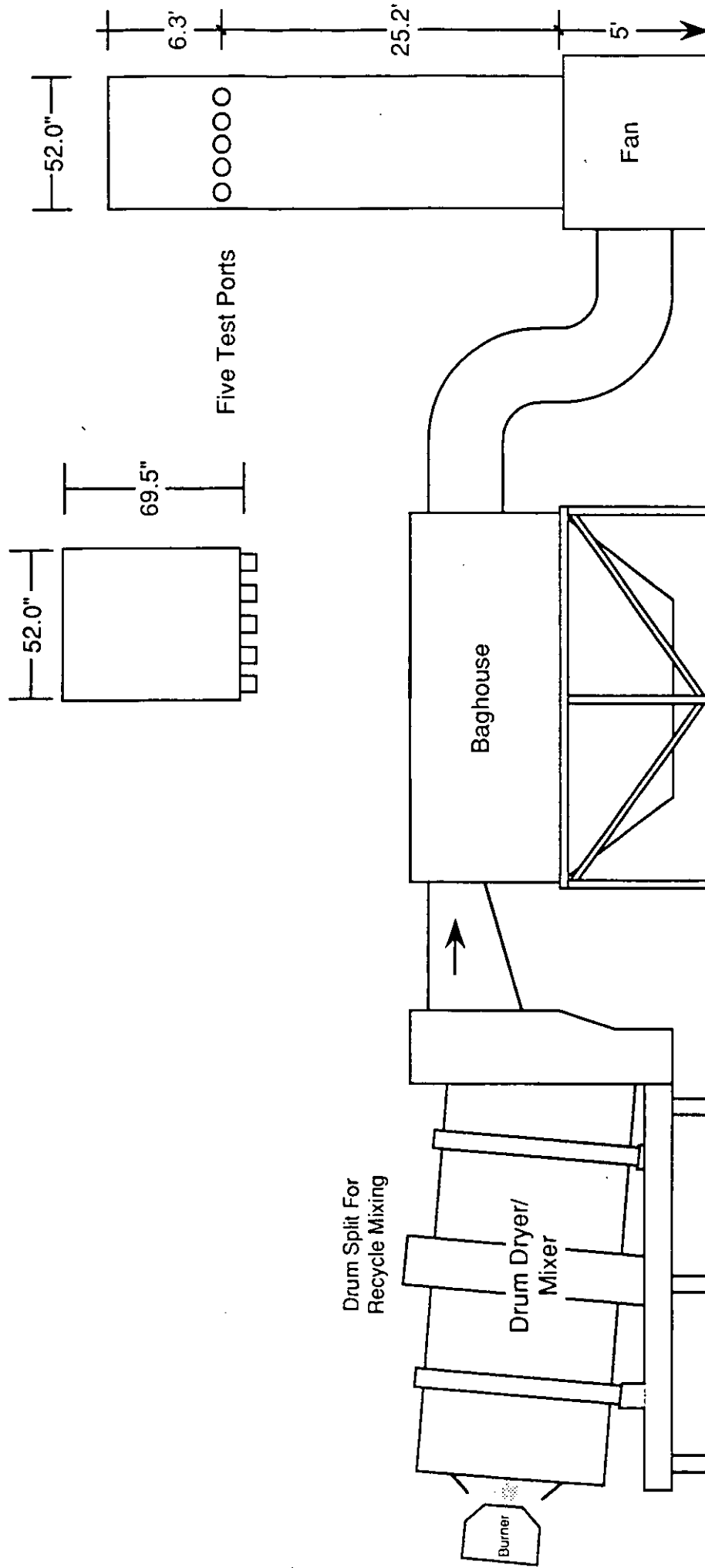
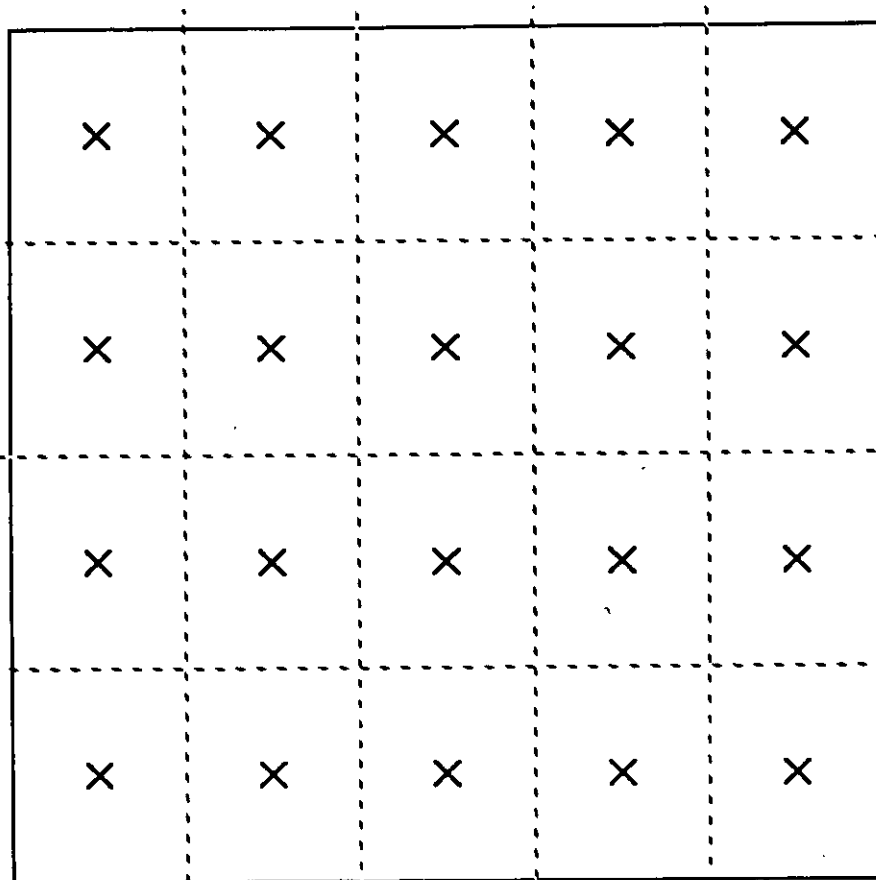


Figure 2

Commercial Asphalt
Company
Ramsey, Minnesota
Baghouse Stack

Location of Traverse Points



Duct Dimensions (Inches)

69.5 x 52.0

Number of Sampling Ports

5

Number of Traverse Points

20

Figure 3

APPENDIX A
Field Data Sheets and Notes

EPA METHODS 2-5 FIELD DATA SHEETS

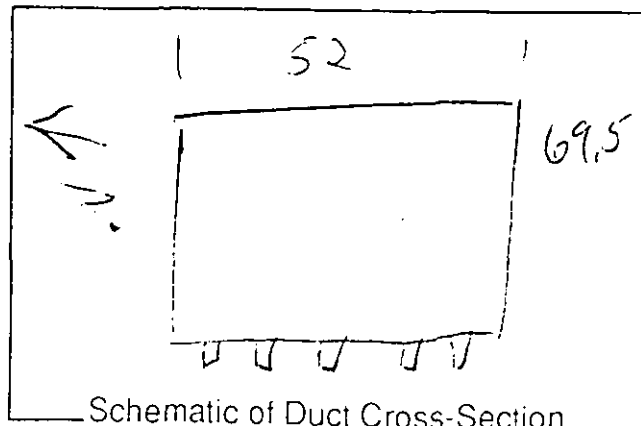
EPA Method 2 Field Data Sheet

Project CA R002.504
Test Location Bayhourse JHlet
Date 9-1-93 Test 1 Run 1
Operators Tom Hockinski Mark G. Olson
Barometric Pressure 29.50 Inches Hg
Static Pressure 4.30 Inches H₂O
Pitot Leak Check - Positive 0.0 Negative 0.0

Pitot Tube No. 10 C_p 0.840
Pressure Measurement Device 0.1 nanometer
Duct Dimensions 69.5 x 52 Inches
Port Length 2.0 Inches
Temp. - Dry Bulb 208 °F, Wet Bulb 164 °F
Moisture Content 12.0 36.0 %
320P Oxygen Concentration 13.0 %
Time of Measurement 1216 (24 Hr. Clock)

Traverse Point Identification				Cyclonic Flow Yaw Angle	Velocity Head ΔP Inches H ₂ O	Stack Temperature ° F
Point Number	% Of Diameter	Inches From:				
		Wall	Port			
E 1		51.69	10.69	°	20	
2		26.26	28.06	°	32	
3		43.44	45.44	°	34	
4		60.81	62.81	°	37	
1				°	26	
2				°	30	
3				°	40	
4				°	45	
1				°	2.64	Avg ΔP:
2				°	39	
3				°	36	
4				°	47	
1				°	53	
2				°	28	
3				°	30	
4				°	36	
1				°	44	
2				°	33	
3				°	36	
4				°	38	
				°	42	
				°		
				°		
				°		
				°		

Avg ΔP = 34
Opt 120
use
Opt 133



Computer Data Summary:

Stack Pressure 21.82 Inches Hg
Duct Area 25.047 Square Feet
Molecular Weight - M_d 29.91
Molecular Weight - M_s 25.62
Avg. Duct Temperature 225 °F
Average √ΔP 0.2965
Flue Gas Velocity 40.73 Feet/Sec.
Volumetric Flow Rate:
ACFM 61325
DSCFM 29359

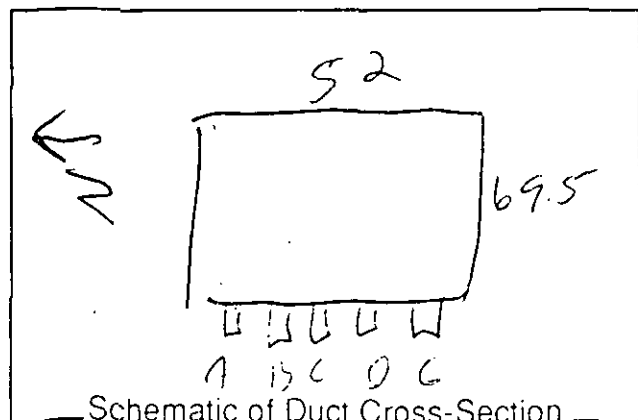
EPA Method 2 Field Data Sheet

Project CA / Ramsey
 Test Location Day Horse Outlet
 Date 4-2-97 Test 1 Run 1
 Operators TAK NEW Mum
 Barometric Pressure 24.16 Inches Hg
 Static Pressure + .22 Inches H₂O
 Pitot Leak Check - Positive _____ Negative _____

Pitot Tube No. 70 C_p .840
 Pressure Measurement Device 0.1 Manometer
 Duct Dimensions 52 X 69.5 Inches
 Port Length 2.0 Inches
 Temp. - Dry Bulb _____ °F, Wet Bulb _____ °F
 Moisture Content _____ %
 320P Oxygen Concentration _____ %
 Time of Measurement 0703 (24 Hr. Clock)

cyclonic at 0635

Traverse Point Identification				Cyclonic Flow Yaw Angle	Velocity Head ΔP Inches H ₂ O	Stack Temperature ° F
Point Number	% Of Diameter	Inches From:				
		Wall	Port			
A	1	8.09	10.64	3 °	58	
	2	26.06	28.06	3 °		
	3	43.44	45.44	3 °		
	4	60.81	62.81	-1 °		
B	1			4 °		
	2			2 °		
	3			-2 °		
	4			0 °		
C	1			-13 °		
	2			-6 °		
	3			5 °		
	4			5 °		
D	1			4 °		
	2			4 °		
	3			5 °		
	4			3 °		
E	1			0 °		
	2			1 °		
	3			2 °		
	4			3 °		
				°		
				°		
				°		



Computer Data Summary:

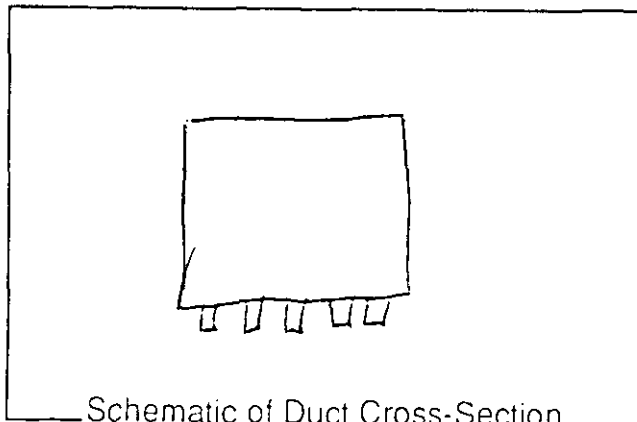
Stack Pressure _____ Inches Hg
 Duct Area _____ Square Feet
 Molecular Weight - M_d _____
 Molecular Weight - M_s _____
 Avg. Duct Temperature _____ °F
 Average √ΔP _____
 Flue Gas Velocity _____ Feet/Sec.
 Volumetric Flow Rate:
 ACFM _____
 DSCFM _____

EPA Method 2 Field Data Sheet

Project CA / Ramsey
Test Location Bughouse outlet
Date 9-93 Test 1 Run 1
Operators TAK MGN
Barometric Pressure 29.16 Inches Hg
Static Pressure _____ Inches H₂O
Pitot Leak Check - Positive 0.0 Negative 0.0

Pitot Tube No. 8 C_p .840
Pressure Measurement Device Diff Manometer
Duct Dimensions 52 x 69.5 Inches
Port Length 2.0 Inches
Temp. - Dry Bulb 234 °F, Wet Bulb 163 °F
Moisture Content 33.0 %
320P Oxygen Concentration _____ %
Time of Measurement 0703 (24 Hr. Clock)

Traverse Point Identification				Cyclonic Flow Yaw Angle	Velocity Head ΔP Inches H ₂ O	Stack Temperature ° F
Point Number	% Of Diameter	Inches From:				
		Wall	Port			
A 1		8.69	10.69	°	.38	
2		26.06	28.06	°	.44.39	
3		43.44	45.44	°	.47	
4		60.81	62.81	°	.50	
B 1				°		
2				°		
3				°		
4				°		
C 1				°		
2				°		
3				°		
4				°		
D 1				°		
2				°		
3				°		
4				°		
E 1				°		
2				°		
3				°		
4				°		
				°		
				°		
				°		
				°		



Computer Data Summary:

Stack Pressure _____ Inches Hg
Duct Area _____ Square Feet
Molecular Weight - M_d _____
Molecular Weight - M_s _____
Avg. Duct Temperature _____ °F
Average √ΔP _____
Flue Gas Velocity _____ Feet/Sec.
Volumetric Flow Rate:
ACFM _____
DSCFM _____

Field Computer Summary

Project Name: CA / Ramsey
Sampling Location: Bughouse Outlet
Date of Test: 9-8-93
Test Number: 1

Operator: Tom K. Kish

Initialization Parameters	Run Specific Input Parameters			
	Run 1	Run 2	Run 3	Run 4
Meter Coef. - α = <u>.9974</u>	V/O <u>439.40</u>	<u>487.90</u>	<u>524.91</u>	<u>571.10</u>
Orif. Coef. - $\Delta H@$ = <u>2.118</u>	No. Of Points <u>20</u>	<u>20</u>	<u>20</u>	<u>20</u>
Pitot Coef. - C_p = <u>.840</u>	MC <u>33.0</u>	<u>34.5</u>	<u>34.9</u>	<u>33.6</u>
Nozzle Dia. - D_n = <u>.311</u>	V/F <u>487.59</u>	<u>524.70</u>	<u>570.81</u>	<u>618.16</u>
Bar. Pres. - P_b = <u>29.16</u>	Grams H_2O <u>520</u>	<u>392</u>	<u>460</u>	<u>500</u>
Time/Point - ΔT = <u>3</u>	Run Time <u>60</u>	<u>60</u>	<u>60</u>	<u>60</u>
Moisture Content = <u>33.0</u>	1-Rnd/2-Rect <u>2</u>	<u>2</u>	<u>2</u>	<u>2</u>
% Oxygen = <u>12.0</u>	Diameter(Ins.)			
Meter Temp. - t_m = <u>61</u>	Length(Ins.) <u>69.5</u>	<u>69.5</u>	<u>69.5</u>	<u>69.5</u>
Static Pres. - P_g = <u>1.22</u>	Width(Ins.) <u>52</u>	<u>52</u>	<u>52</u>	<u>52</u>
End Of Run Summary				
	Run 1	Run 2	Run 3	Run 4
Avg. $\sqrt{\Delta P}$	<u>.722</u>	<u>.716</u>	<u>.683</u>	<u>.685</u>
Avg. ΔH	<u>2.363</u>	<u>2.337</u>	<u>2.056</u>	<u>2.159</u>
Avg. t_s	<u>222.35</u>	<u>231.94</u>	<u>241.40</u>	<u>242.30</u>
Avg. t_m	<u>70.78</u>	<u>90.38</u>	<u>93.18</u>	<u>92.23</u>
Standard Vol.	<u>46.88</u>	<u>34.52</u>	<u>42.81</u>	<u>43.98</u>
Moist. Content	<u>34.30</u>	<u>34.83</u>	<u>37.59</u>	<u>34.86</u>
Avg. Gas Vel.	<u>49.44</u>	<u>49.31</u>	<u>47.53</u>	<u>47.44</u>
% Isokinetic	<u>100.78</u>	<u>101.64</u>	<u>97.35</u>	<u>102.28</u>
ACFM	<u>74445</u>	<u>74251</u>	<u>71562</u>	<u>71430</u>
DSCFM	<u>36904</u>	<u>36005</u>	<u>34886</u>	<u>34112</u>

EPA Method 5 Field Data Sheet

Project CA Ramsey
 Sample Location Bughouse Outlet
 Date 5-6-93 Test 1 Run 2
 Operators Jack New
 Train No. 6m-6 Pitot Tube No. 8 C_p .840 Sampling Train Leak Checks:
 Meter Coef. .9974 Bar. Pres. 29.16 Ins. Hg Pretest 0.00 @ 15 Ins. Hg
 Orifice Coef. ΔH @ 1.118 Static Pres. +22 Ins. H₂O Posttest 0.00 @ 1.0 Ins. Hg
 Nozzle No. 2-3 D_n 34 Estimated MC 34.5 % Pitot Positive 0.0 Negative 0.0

[illegible]

Samples Recovered: Filter No. 2919 ; ☒ Probe Wash; ☒ Wet Catch; ☐ Other _____

Integrated Gas Sampling Data: _____

Moisture Recovery Data: _____

* 1038 fire vent out in process
1105 restart 35.7
1108 fire out 35.7
1124 restart

Box No. 7 Bag Material 12/15 Impinger No. Bulb

Bag No. 2 Leak Checks 2.2 cc/min. @ 25"Hg Final Volume 304

Bag Vol. 40 Liters Posttest O₂ Reading _____ Initial Volume 100

320 P No. _____ Difference 204

1	2	3	4	Desiccant	Total
304	267	3	X	14.5	
100	100	0	X	13.8	
204	167	3	X	17	392

EPA Method 5 Field Data Sheet

Project CA Ramsey
Sample Location Bighouse O.Het
Date 9-8-93 Test 1 Run 3
Operators TAK MCW
Train No. CM-6-24345-1
Meter Coef. 0.9974
Orifice Coef. ΔH@2.118
Nozzle No. 2-3 D_n 3.11
Pitot Tube No. 7 C_p .840
Bar. Pres. 29.16 Ins. Hg
Static Pres. 1.22 Ins. H₂O
Estimated MC 37.9 %
Sampling Train Leak Checks:
Pretest 0.00 @ 15 Ins. Hg
Posttest 0.00 @ 9.5 Ins. Hg
Pitot Positive 0.1 Negative 0.0

Point No.	Time ΔT	Meter Vol. V _m Cubic Feet	Velocity Head - ΔP Inches WC	Orifice Meter - ΔH Inches WC	Desired ΔV _m	Desired V _m	Vacuum Inches Hg	Stack Temp. ° F	Sampling Train Temperatures · °F					320 P Oxygen Percent
									Filter	Probe	Impinger Outlet	Meter Inlet	Meter Outlet	
4	3	527.26	50	2.21	238	729	4.3	243	244	260	60	88	88	w
3	6	529.64	50	2.25	241	970	4.5	252	246	261	64	89	88	
2	9	534.98	48	2.08	231	201	4.2	252	249	254	61	92	88	
1	12	539.01	39	1.49	196	397	3.5	247	242	241	63	94	88	w=37
4	15	536.51	54	2.48	253	650	4.9	239	246	252	66	94	88	
3	18	538.94	57	2.37	247	848	4.8	245	237	261	58	96	88	
2	21	541.24	49	2.04	230	137	4.5	246	249	258	57	97	88	
1	24	543.55	40	1.67	208	335	3.9	245	251	241	59	98	88	w=34
4	27	546.00	62	2.84	271	606	5.5	237	239	254	63	98	89	
3	30	548.54	53	2.44	254	860	5.3	245	251	263	58	99	89	w=55
2	33	550.80	43	1.87	220	081	4.5	245	248	253	58	100	89	
1	36	552.90	39	1.70	210	291	4.1	245	249	247	58	101	89	
4	39	555.47	57	2.54	257	548	5.2	232	230	241	62	99	90	
3	42	557.86	53	2.32	246	744	5.1	240	244	263	57	100	90	
2	45	560.19	49	1.93	224	017	4.5	242	246	254	58	101	90	
1	48	562.50	43	1.89	222	229	4.3	241	248	245	56	101	90	
4	51	564.05	27	1.23	179	418	3.1	215	249	264	61	100	90	
3	54	566.03	33	1.46	195	613	3.9	239	250	262	56	99	90	w=36
2	57	568.32	48	2.08	232	846	5.0	241	249	250	57	100	90	
1	60	570.81	50	2.16	237	083	5.2	242	248	239	58	101	90	
	(1202)													
O = 60		V _m = 45.40	.683	ΔH = .056				T _s = 241.40					T _m = 92.6	

Samples Recovered: Filter No. _____; ☒ Probe Wash; ☒ Wet Catch; ☐ Other _____

Integrated Gas Sampling Data: _____

Moisture Recovery Data: _____

Box No. 4 Bag Material Tecelaw
 Bag No. 3 Leak Checks 0.0 cc/min. @ 25"Hg
 Bag Vol. 20.0 Liters Posttest O₂ Reading _____
 320 P No. _____

1	2	3	4	Desiccant	Total
310	332	4	X	1366	
160	100	0		1352	
310	232	4	X	14	860

Impinger No. _____
 Final Volume _____
 Initial Volume _____
 Difference _____

9

2025

2000

Company: CA / Ramsey

Date(s): 9-8-93

Project No.: 930831.401

Significant Events & Notes

1) Arrived at 0600
Ready to test at 0650

2) Start R1 at 0715
Finish at 0824

3) waited for process for R2 to start
Start at 1000

4) Flame out on Burner stop at 1038 Restart at
1105 stop at 1108 run No good

5) since run (2) will not be acceptable for compliance
oil from one and two should be analyzed for run 1
or a portion taken from it for combined sample
I mixed them together midway through R2 before problems

6) waited for process until 1251 they had to mix
something else for about 45 min Begin R3 at 1251

7) During the last port change of run #3 I accidentally scrapped the pitot tubes
against the stack wall. I saw the pitot tubes come into contact with the stack
through the port hole. I also noticed that the nozzle did not touch

the stack wall. Furthermore the nozzle could not of touched the stack
wall because the port change that took place was the far left port which
and the pitot tubes were on that side of the probe. The pitot tubes

were between the stack wall and the nozzle during the time that the
pitot tubes scrapped the stack wall. When I scrapped the stack I told
Tom Kuchinski about the incident.

8) The client made a comment when the
incident occurred but after the run
seemed to understand what happened.

Made by W. Wilson
9/8/93

11)

Diagram of
Incident. stack
wall

Pitot tube
nozzle



EPA METHOD 9 FIELD DATA SHEETS

EPA Method 9 Field Data Sheet

Project CIA Ramsey
Source No. 1 I.D. Baghouse stack
Source No. 2 I.D. _____
Test No. 1

Evaluation Date 9-8-93
Observer M. Loftus
Certification Date 3-31-93

Source No. 1 Asphalt
Type of Source MFG. Control Device Baghouse
Fuel Type Waste oil Load 600 TPH

Source No. 2
Type of Source _____ Control Device _____
Fuel Type _____ Load _____

Source Height(s) ~50ft Outlet Dimensions 52"x69.5"

Plume Description:

Type ☐ Coning ☐ Fanning ☐ Looping ☒ Lofting ☐ Fumigating
Color Whitish Brown Length 150-175 ft
Steam Plume ☒ Attached ☐ Detached ☐ No Visible Steam

Background Description (Type, color) Blue sky

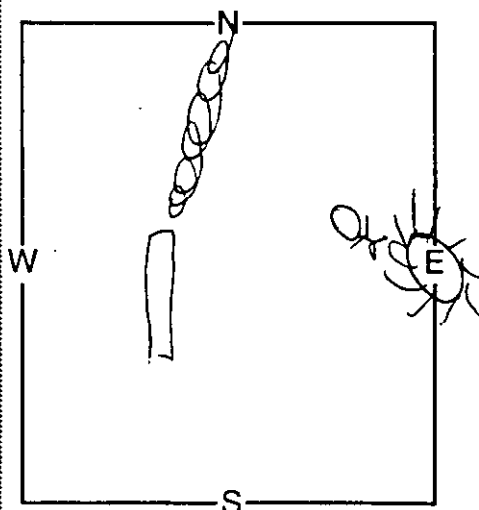
Meteorological Conditions (clear, % cloudy, etc.) clear

Wind Direction from SSW Speed 5-10 mph
Ambient Temp. 55 °F

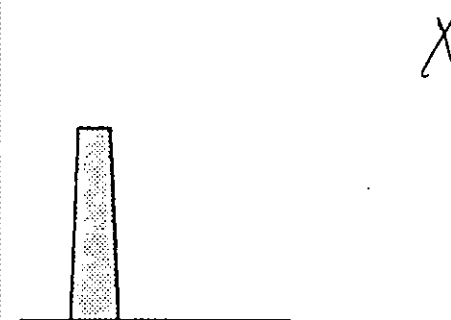
Location of Observer (direction and distance) EAST 400ft

Personnel Present During Observation none

Show Observer's Position
In Relation to the Source,
Plume and Lighting



Show Point Where Readings
Were Evaluated In Relation
to the Source Outlet and
the Steam Plume



Comments (include any changes to the above during evaluation) _____

VISIBLE EMISSION EVALUATOR CERTIFICATION

VISIBLE EMISSIONS EVALUATOR

This is to certify that

Mike Lofton

met the specifications of Federal Reference Method 9 and qualified as a visible emissions evaluator. Maximum deviation on white and black smoke did not exceed 7.5% opacity and no single error exceeding 15% opacity was incurred during the certification test conducted by Eastern Technical Associates of Raleigh, North Carolina. This certificate is valid for six months from date of issue.

Thermon Lane
President

Will S. [Signature]
Vice President

David B. Savage, Jr.
Program Manager

238352
Certificate Number

Munroeopolis
Location

April 1, 1993
Date of Issue

APPENDIX B
Laboratory Data and Reports

EPA Method 3 Laboratory Summary Sheet

Project LA Runway Analyst Al. Wilson
 Sampling Location Baghouse Outlet Analysis Date 9/9/93
 Sampling Date 9/8/93 Apparatus Leak Check - Pos. 0.0 Neg. 0.0
 Project Number 930831.401 Apparatus Identification CB-C1
 Sample Type ☒ Integrated ☒ Grab

Test No.	Run No.	Orsat Analyzer Results			F _o	O ₂ Analyzer Results		Sample Container
		% CO ₂	% O ₂	% CO		Field	Lab	
1	0	0.00	20.90		—	—	—	☐ Tedlar™ Bag ☐ Glass Bulb
1	1	6.50	12.40		1.308	—	12.1	☒ Tedlar™ Bag ☐ Glass Bulb
1	3	7.75	10.80		1.303	—	10.3	☒ Tedlar™ Bag ☐ Glass Bulb
1	4	7.70	10.70		1.325	—	10.4	☒ Tedlar™ Bag ☐ Glass Bulb
1	2	6.05	11.38		1.574	—	—	☐ Tedlar™ Bag ☒ Glass Bulb
								☐ Tedlar™ Bag ☐ Glass Bulb
								☐ Tedlar™ Bag ☐ Glass Bulb
								☐ Tedlar™ Bag ☐ Glass Bulb
								☐ Tedlar™ Bag ☐ Glass Bulb
								☐ Tedlar™ Bag ☐ Glass Bulb

Calculate F_o before evacuating any samples. Compare F_o to expected fuel values. If discrepancies exist, reanalyze samples. Calculate F_o as follows:

$$F_o = \frac{20.9 - \% O_2}{\% CO_2}$$

Comments Field O₂ readings
could not be taken due
to analyzer problem.

F _o Ranges For Common Fuels	
Anthracite Coal & Lignite	1.016 - 1.130
Bituminous Coal	1.083 - 1.230
Distillate Oil	1.260 - 1.413
Residual Oil	1.210 - 1.370
Wood	1.000 - 1.120
Wood Bark	1.003 - 1.130
Natural Gas	1.600 - 1.836
Propane	1.434 - 1.586
Butane	1.405 - 1.553

EPA Method 3 Laboratory Data Sheet

Project C1 Ramsey Analyst M. Wilson
 Sampling Location Baghouse Outlet Analysis Date 9/9/93
 Sampling Date 9/8/93 Apparatus Leak Check - Pos. 0.0 Neg. 0.0
 Project Number 930831.101 Apparatus Identification CB-01

Test <u>1</u> Run <u>0</u>	Aliquot Volume Zero Point <u>0.00</u> ml Sample Volume <u>100.00</u> ml	CO ₂ Initial Reading <u>0.00</u> ml Final Reading <u>0.00</u> ml Volume CO ₂ <u>0.00</u> ml % CO ₂ <u>0.00</u> %	O ₂ Initial Reading <u>0.00</u> ml Final Reading <u>20.90</u> ml Volume O ₂ <u>20.90</u> ml % O ₂ <u>20.90</u> %
Duplicate	Aliquot Volume Zero Point _____ ml Sample Volume _____ ml	CO ₂ Initial Reading _____ ml Final Reading _____ ml Volume CO ₂ _____ ml % CO ₂ _____ %	O ₂ Initial Reading _____ ml Final Reading _____ ml Volume O ₂ _____ ml % O ₂ _____ %
Average		% CO ₂ _____ %	% O ₂ _____ %
Test <u>1</u> Run <u>1</u>	Aliquot Volume Zero Point <u>0.00</u> ml Sample Volume <u>100.00</u> ml	CO ₂ Initial Reading <u>0.00</u> ml Final Reading <u>6.40</u> ml Volume CO ₂ <u>6.40</u> ml % CO ₂ <u>6.40</u> %	O ₂ Initial Reading <u>6.40</u> ml Final Reading <u>13.90</u> ml Volume O ₂ <u>12.50</u> ml % O ₂ <u>12.50</u> %
Duplicate	Aliquot Volume Zero Point <u>0.00</u> ml Sample Volume <u>100.00</u> ml	CO ₂ Initial Reading <u>0.00</u> ml Final Reading <u>6.60</u> ml Volume CO ₂ <u>6.60</u> ml % CO ₂ <u>6.60</u> %	O ₂ Initial Reading <u>6.60</u> ml Final Reading <u>13.90</u> ml Volume O ₂ <u>12.30</u> ml % O ₂ <u>12.30</u> %
Average		% CO ₂ <u>6.50</u> %	% O ₂ <u>12.40</u> %

Comments: _____

EPA Method 3 Laboratory Data Sheet

Project LA Ramsey Analyst M. Wilson
 Sampling Location Bughouse Ditch Analysis Date 9/9/93
 Sampling Date 9/9/93 Apparatus Leak Check - Pos. 0.0 Neg. 0.0
 Project Number 930831 401 Apparatus Identification 06-01

Test <u>1</u> Run <u>2</u>	Aliquot Volume Zero Point <u>4.30</u> ml Sample Volume <u>95.40</u> ml	CO_2 Initial Reading <u>4.30</u> ml Final Reading <u>10.50</u> ml Volume CO_2 <u>6.20</u> ml % CO_2 <u>6.20</u> % <u>5.93</u>	O_2 Initial Reading <u>10.50</u> ml Final Reading <u>22.30</u> ml Volume O_2 <u>11.80</u> ml % O_2 <u>11.29</u> %
Duplicate	Aliquot Volume Zero Point <u>2.00</u> ml Sample Volume <u>98.00</u> ml	CO_2 Initial Reading <u>2.00</u> ml Final Reading <u>8.30</u> ml Volume CO_2 <u>6.30</u> ml % CO_2 <u>6.17</u> %	O_2 Initial Reading <u>5.30</u> ml Final Reading <u>20.00</u> ml Volume O_2 <u>11.70</u> ml % O_2 <u>11.47</u> %
Average		% CO_2 <u>6.05</u> %	% O_2 <u>11.38</u> %
Test _____ Run _____	Aliquot Volume Zero Point _____ ml Sample Volume _____ ml	CO_2 Initial Reading _____ ml Final Reading _____ ml Volume CO_2 _____ ml % CO_2 _____ %	O_2 Initial Reading _____ ml Final Reading _____ ml Volume O_2 _____ ml % O_2 _____ %
Duplicate	Aliquot Volume Zero Point _____ ml Sample Volume _____ ml	CO_2 Initial Reading _____ ml Final Reading _____ ml Volume CO_2 _____ ml % CO_2 _____ %	O_2 Initial Reading _____ ml Final Reading _____ ml Volume O_2 _____ ml % O_2 _____ %
Average		% CO_2 _____ %	% O_2 _____ %

Comments: _____

EPA Method 3 Laboratory Data Sheet

Project CA Ramsey Analyst M. Wilson
 Sampling Location Baghouse Outlet Analysis Date 9/9/93
 Sampling Date 9/5/93 Apparatus Leak Check - Pos. C.C Neg. C.C
 Project Number 930931401 Apparatus Identification CB-C1

Test <u>1</u> Run <u>3</u>	Aliquot Volume Zero Point <u>0.00</u> ml <u>100.00</u> Sample Volume <u> </u> ml	CO ₂ Initial Reading <u>0.00</u> ml Final Reading <u>7.70</u> ml Volume CO ₂ <u>7.70</u> ml % CO ₂ <u>7.70</u> %	O ₂ Initial Reading <u>7.70</u> ml Final Reading <u>18.60</u> ml Volume O ₂ <u>10.90</u> ml % O ₂ <u>10.90</u> %
Duplicate	Aliquot Volume Zero Point <u>0.00</u> ml <u>100.00</u> Sample Volume <u> </u> ml	CO ₂ Initial Reading <u>0.00</u> ml Final Reading <u>7.80</u> ml Volume CO ₂ <u>7.80</u> ml % CO ₂ <u>7.80</u> %	O ₂ Initial Reading <u>7.80</u> ml Final Reading <u>18.50</u> ml Volume O ₂ <u>10.70</u> ml % O ₂ <u>10.70</u> %
Average		% CO ₂ <u>7.75</u> %	% O ₂ <u>10.80</u> %
Test <u>1</u> Run <u>4</u>	Aliquot Volume Zero Point <u>0.00</u> ml <u>100.00</u> Sample Volume <u> </u> ml	CO ₂ Initial Reading <u>0.00</u> ml Final Reading <u>7.60</u> ml Volume CO ₂ <u>7.60</u> ml % CO ₂ <u>7.60</u> %	O ₂ Initial Reading <u>7.60</u> ml Final Reading <u>18.40</u> ml Volume O ₂ <u>10.80</u> ml % O ₂ <u>10.80</u> %
Duplicate	Aliquot Volume Zero Point <u>0.00</u> ml <u>100.00</u> Sample Volume <u> </u> ml	CO ₂ Initial Reading <u>0.00</u> ml Final Reading <u>7.80</u> ml Volume CO ₂ <u>7.80</u> ml % CO ₂ <u>7.80</u> %	O ₂ Initial Reading <u>7.80</u> ml Final Reading <u>18.40</u> ml Volume O ₂ <u>10.60</u> ml % O ₂ <u>10.60</u> %
Average		% CO ₂ <u>7.70</u> %	% O ₂ <u>10.70</u> %

Comments: _____

PARTICULATE ANALYTICAL DATA



INORGANIC LABORATORY

EPA Method 5 Particulate Gravimetric Sheet
Organic Condensibles

Project Commercial Asphalt Analyst BOL
Sampling Location Baghouse Outlet Analysis Date(s) 9-14-93
Sampling Date 9-8-93 Sampling Reagent OI
Test Number 1 LDMS Entry _____ Initials _____
Project Number 930909.505 LDMS Validation 9-16-93 Initials JMC
1043417

Sample No. 22973.3
Run Number 1
Dish Number Z2
Vol 1 350 > 750
2 400
Date/Time 9-16-93 0900
Gross Weight 98.4895 g

Date/Time 9-16-93 1330
Gross Weight 98.4899 g

Avg. Gross Wt. 98.4897 g
Dish Tare Wt. 98.4824 g
Difference 0.0073 g

Blank Weight -0.0017 g

Condensible
Organic Wt. 0.0073 g

Transfer "Condensible Organic
Wt." to Box Number 1.

WC 1 0.0073 g

Sample No. 22974.1
Run Number 2
Dish Number MAck
Vol 1 250 > 550
2 300
Date/Time 9-16-93 0900
Gross Weight 112.3277 g

Date/Time 9-16-93 1330
Gross Weight 112.3281 g

Avg. Gross Wt. 112.3279 g
Dish Tare Wt. 112.3218 g
Difference 0.0061 g

Blank Weight -0.0017 g

Condensible
Organic Wt. 0.0061 g

Transfer "Condensible Organic
Wt." to Box Number 2.

WC 2 0.0061 g

Sample No. 22975.0
Run Number 3
Dish Number Carol
Vol 1 300 > 700
2 400
Date/Time 9-16-93 0900
Gross Weight 100.6262 g

Date/Time 9-16-93 1330
Gross Weight 100.6266 g

Avg. Gross Wt. 100.6264 g
Dish Tare Wt. 100.6157 g
Difference 0.0107 g

Blank Weight -0.0017 g

Condensible
Organic Wt. 0.0107 g

Transfer "Condensible Organic
Wt." to Box Number 3.

WC 3 0.0107 g



INORGANIC LABORATORY

EPA Method 5 Particulate Gravimetric Sheet
Organic Condensibles

Project Commercial Asphalt Analyst BDL
Sampling Location Baghouse Outlet Analysis Date(s) 9-14-93
Sampling Date 9-8-93 Sampling Reagent DI
Test Number 1 LDMS Entry _____ Initials _____
Project Number 930909.505 LDMS Validation 9-16-93 Initials PMC

Sample No. 22976.8
Run Number 4
Dish Number 617
Vol 1 340
2 350
Date/Time 9-16-93 0900
Gross Weight 113.9066 g

Date/Time 9-16-93 1330
Gross Weight 113.9065 g

Avg. Gross Wt. 113.9066 g
Dish Tare Wt. 113.8976 g
Difference ~~0.0106~~ g
0.0090

Blank Weight -0.0017 g

Condensible 0.0090
Organic Wt. ~~0.0106~~ g

Transfer "Condensible Organic Wt." to Box Number 1.

WC 1 0.0090
~~0.0106~~ g

Sample No. _____
Run Number _____
Dish Number _____
Date/Time _____
Gross Weight _____ g

Date/Time _____
Gross Weight _____ g

Avg. Gross Wt. _____ g
Dish Tare Wt. _____ g
Difference _____ g

Blank Weight _____ g

Condensible _____
Organic Wt. _____ g

Transfer "Condensible Organic Wt." to Box Number 2.

WC 2 _____ g

Sample No. _____
Run Number _____
Dish Number _____
Date/Time _____
Gross Weight _____ g

Date/Time _____
Gross Weight _____ g

Avg. Gross Wt. _____ g
Dish Tare Wt. _____ g
Difference _____ g

Blank Weight _____ g

Condensible _____
Organic Wt. _____ g

Transfer "Condensible Organic Wt." to Box Number 3.

WC 3 _____ g



INORGANIC LABORATORY

EPA Method 5 Particulate Gravimetric Sheet

Particulate In Probe Wash

Project Commercial Asphalt Analyst BDL
Sampling Location Baghouse Outlet Analysis Date(s) 9-14-93
Sampling Date 9-8-93 Cleanup Reagent(s) Acetone
Test Number 1 LDMS Entry _____ Initials _____
Project Number 930909.505 LDMS Validation 9-16-93 Initials Jmc

Sample No. <u>22973.3</u>	Sample No. <u>22974.1</u>	Sample No. <u>22975.0</u>
Run Number <u>1</u>	Run Number <u>2</u>	Run Number <u>3</u>
Dish Number <u>DR3</u>	Dish Number <u>Pux</u>	Dish Number <u>Boy</u>
Reagent Vol. <u>125</u> ml	Reagent Vol. <u>140</u> ml	Reagent Vol. <u>155</u> ml
Date/Time <u>9-16-93 0900</u>	Date/Time <u>9-16-93 0900</u>	Date/Time <u>9-16-93 0900</u>
Gross Weight <u>103.5766</u> g	Gross Weight <u>98.4912</u> g	Gross Weight <u>106.5559</u> g
Date/Time <u>9-16-93 1330</u>	Date/Time <u>9-16-93 1330</u>	Date/Time <u>9-16-93 1330</u>
Gross Weight <u>103.5770</u> g	Gross Weight <u>98.4916</u> g	Gross Weight <u>106.5564</u> g
Avg. Gross Wt. <u>103.5768</u> g	Avg. Gross Wt. <u>98.4914</u> g	Avg. Gross Wt. <u>106.5562</u> g
Dish Tare Wt. <u>103.5339</u> g	Dish Tare Wt. <u>98.4573</u> g	Dish Tare Wt. <u>106.5233</u> g
Difference <u>0.0429</u> g	Difference <u>0.0341</u> g	Difference <u>0.0329</u> g
Blank Weight <u>-0.0022</u> g	Blank Weight <u>-0.0022</u> g	Blank Weight <u>-0.0022</u> g
Particulate In Rinse Weight <u>0.0429</u> g	Particulate In Rinse Weight <u>0.0341</u> g	Particulate In Rinse Weight <u>0.0329</u> g
Transfer "Particulate In Rinse Weight" to Box Number 1.	Transfer "Particulate In Rinse Weight" to Box Number 2.	Transfer "Particulate In Rinse Weight" to Box Number 3.
PW 1 <u>0.0429</u> g	PW 2 <u>0.0341</u> g	PW 3 <u>0.0329</u> g



INORGANIC LABORATORY

EPA Method 5 Particulate Gravimetric Sheet
Particulate In Probe Wash

Project Commercial Asphalt Analyst BDL
Sampling Location Baghouse Analysis Date(s) 9-14-93
Sampling Date 9-8-93 Cleanup Reagent(s) Acetone
Test Number 1 LDMS Entry _____ Initials _____
Project Number 930909.505 LDMS Validation 9-16-93 Initials Jme

Sample No. <u>22976.8</u>	Sample No. _____	Sample No. _____
Run Number <u>4</u>	Run Number _____	Run Number _____
Dish Number <u>PR</u>	Dish Number _____	Dish Number _____
Reagent Vol. <u>PR 150</u> ml <u>BDL</u> <u>9-14-93</u>	Reagent Vol. _____ ml	Reagent Vol. _____ ml
Date/Time <u>9-16-93 0900</u>	Date/Time _____	Date/Time _____
Gross Weight <u>99.9192</u> g	Gross Weight _____ g	Gross Weight _____ g
Date/Time <u>9-16-93 1330</u>	Date/Time _____	Date/Time _____
Gross Weight <u>99.9196</u> g	Gross Weight _____ g	Gross Weight _____ g
Avg. Gross Wt. <u>99.9194</u> g	Avg. Gross Wt. _____ g	Avg. Gross Wt. _____ g
Dish Tare Wt. <u>99.8870</u> g	Dish Tare Wt. _____ g	Dish Tare Wt. _____ g
Difference <u>0.0324</u> g	Difference _____ g	Difference _____ g
Blank Weight <u>-0.0022</u> g	Blank Weight _____ g	Blank Weight _____ g
Particulate In Rinse Weight <u>0.0324</u> g	Particulate In Rinse Weight _____ g	Particulate In Rinse Weight _____ g
Transfer "Particulate In Rinse Weight" to Box Number 1.	Transfer "Particulate In Rinse Weight" to Box Number 2.	Transfer "Particulate In Rinse Weight" to Box Number 3.
PW 1 <u>0.0324</u> g	PW 2 _____ g	PW 3 _____ g

EPA Method 5 Particulate Gravimetric Sheet

Particulate On Filter

Project Commercial Asphalt Analyst BOL
 Sampling Location Baghouse Outlet Analysis Date(s) 9-14-93
 Sampling Date 9-8-93 Filter Type Fiberglass
 Test Number 1 LDMS Entry _____ Initials _____
 Project Number 930909.505 LDMS Validation 9-16-93 Initials Jme

Sample No. <u>22973.3</u>	Sample No. <u>22974.1</u>	Sample No. <u>22975.0</u>
Run Number <u>1</u>	Run Number <u>2</u>	Run Number <u>3</u>
Filter Number <u>29812918</u> <u>BOL 9-14-93</u>	Filter Number <u>2919</u>	Filter Number <u>2921</u>
Date/Time <u>9-14-93 0800</u>	Date/Time <u>9-15-93 1000</u>	Date/Time <u>9-14-93 0800</u>
Gross Weight <u>0.68678</u> g	Gross Weight <u>0.68586</u> g	Gross Weight <u>0.68766</u> g
Date/Time <u>9-14-93 1400</u>	Date/Time <u>9-15-93 1600</u>	Date/Time <u>9-15-93 1600</u>
Gross Weight <u>0.68674</u> g	Gross Weight <u>0.68582</u> g	Gross Weight <u>0.68763</u> g
Avg. Gross Wt. <u>0.68676</u> g	Avg. Gross Wt. <u>0.68584</u> g	Avg. Gross Wt. <u>0.68764</u> g
Filter Tare Wt. <u>0.6736</u> g	Filter Tare Wt. <u>0.6808</u> g	Filter Tare Wt. <u>0.6758</u> g
Difference <u>0.01316</u> g	Difference <u>0.00504</u> g	Difference <u>0.01184</u> g
Particulate On Filter Weight <u>0.01316</u> g	Particulate On Filter Weight <u>0.00504</u> g	Particulate On Filter Weight <u>0.01184</u> g
Transfer "Particulate On Filter Weight" to Box Number 1.	Transfer "Particulate On Filter Weight" to Box Number 2.	Particulate On Filter Weight" to Box Number 3.
Sum particulate weights from each box labeled "1" and record in box labeled "T1."	Sum particulate weights from each box labeled "2" and record in box labeled "T2."	Sum particulate weights from each box labeled "3" and record in box labeled "T3."
AF 1 <u>0.01316</u> g	AF 2 <u>0.00504</u> g	AF 3 <u>0.01184</u> g
Total T1 <u>0.06336</u> g	Total T2 <u>0.04524</u> g	Total T3 <u>0.05544</u> g

EPA Method 5 Particulate Gravimetric Sheet

Particulate On Filter

Project Commercial Asphalt Analyst BOL
 Sampling Location Baghouse Outlet Analysis Date(s) 9-14-92
 Sampling Date 9-8-93 Filter Type Fiberglass
 Test Number 1 LDMS Entry _____ Initials _____
 Project Number 930909.505 LDMS Validation 9-16-93 Initials [Signature]

Sample No. <u>22976.8</u>	Sample No. <u>22977.6</u>	Sample No. _____
Run Number <u>4</u>	Run Number <u>0</u>	Run Number _____
Filter Number <u>2894</u>	Filter Number <u>2902</u>	Filter Number _____
Date/Time <u>9-14-93 0800</u>	Date/Time <u>9-14-93 0800</u>	Date/Time _____
Gross Weight <u>0.68779</u> g	Gross Weight <u>0.67095</u> g	Gross Weight _____ g
Date/Time <u>9-14-93 1400</u>	Date/Time <u>9-14-93 1400</u>	Date/Time _____
Gross Weight <u>0.68775</u> g	Gross Weight <u>0.67100</u> g	Gross Weight _____ g
Avg. Gross Wt. <u>0.68777</u> g	Avg. Gross Wt. <u>0.67098</u> g	Avg. Gross Wt. _____ g
Filter Tare Wt. <u>0.67534</u> g	Filter Tare Wt. <u>0.67040</u> g	Filter Tare Wt. _____ g
Difference <u>0.01243</u> g	Difference <u>0.00058</u> g	Difference _____ g
Particulate On Filter Weight <u>0.01243</u> g	Particulate On Filter Weight <u>0.00058</u> g	Particulate On Filter Weight _____ g
Transfer "Particulate On Filter Weight" to Box Number 1.	Transfer "Particulate On Filter Weight" to Box Number 2.	Particulate On Filter Weight" to Box Number 3.
Sum particulate weights from each box labeled "1" and record in box labeled "T1."	Sum particulate weights from each box labeled "2" and record in box labeled "T2."	Sum particulate weights from each box labeled "3" and record in box labeled "T3."
AF 1 <u>0.01243</u> g	AF 2 <u>0.00058</u> g	AF 3 _____ g
Total T1 <u>0.05543</u> g	Total T2 <u>0.00058</u> g	Total T3 _____ g

0.05323

EPA Method 5 Particulate Gravimetric Sheet

Reagent Blanks

Project Commercial Asphalt Analyst BDL
Sampling Location Baghouse Outlet Analysis Date(s) 7-14-93
Sampling Date 7-8-93
Test Number 1
Project Number 930909.505

Wet Catch

Type: ☐ Organic Condensibles (Extract.)
☐ Inorganic (Residual)
☐ Other _____
☐ Retain For Further Analyses

TPI

Reagent _____
Volume 700 ml

Date/Time 7-16-93 0900
Gross Weight 114.9352 g

Date/Time 7-16-93 1330
Gross Weight 114.9356 g

Avg. Gross Wt. 114.9354 g

Dish Tare Wt. 114.9371 g

Difference -0.0017 g

Blank Weight -0.0017 g

Probe Wash

Type: ☒ Gravimetric
☐ Other _____
☐ Retain For Further Analyses

Reagent 20-200
Volume 100 ml

Date/Time 7-16-93 0900
Gross Weight 113.9061 g

Date/Time 7-16-93 1330
Gross Weight 113.9066 g

Avg. Gross Wt. 113.9064 g

Dish Tare Wt. 113.9076 g

Difference -0.0012 g

Blank Weight -0.0012 g

AGGREGATE ANALYTICAL DATA



REPORT OF LABORATORY ANALYSIS

Commercial Asphalt Company
P.O. Box 1480
Maple Grove, MN 55311-6480

September 30, 1993
PACE Project Number: 930909505

Attn: Ms. Sue Turner

Client Reference: CA/Ramsey/Compliance

PACE Sample Number:

Date Collected:

Time Collected:

Date Received:

Client Sample ID:

10 0229695 10 0229709 10 0229717

09/08/93 09/08/93 09/08/93

07:50 10:30 13:21

09/09/93 09/09/93 09/09/93

Baghouse Baghouse Baghouse

Outlet Outlet Outlet

Parameter

Units

MDI

TIR1 mix

TIR2 mix

TIR3 mix

INORGANIC ANALYSIS

INDIVIDUAL PARAMETERS

Moisture content

%

0.1

3.0

5.0

5.1

SUBCONTRACT LABORATORY REPORT



LABORATORIES, Inc.

P.O. BOX 1873, 1411 S. 12th STREET
BISMARCK, ND 58502
PHONE (701) 258-9720 WATS (800) 279-6885 FAX (701) 258-9724



WE ARE AN EQUAL OPPORTUNITY EMPLOYER

FINAL ANALYSIS REPORT

Sample Number: 93-079

Report Date: 10/ 1/93

Mary Jo Connelly
PACE, Incorporated
1710 Douglas Drive North
Minneapolis, MN 55422

Work Order #: 81-0558
PO #: Pace#930909.505

Date Received: 9/14/93

Sample Description: Oil Sample
Sample Site: #22978.4
Sample Location: Commercial Asphalt Company

Collection Date: 9/ 8/93

Analyte	Results	Units
pH	6.6	units
Lead Waste Oil	44.8	mg/kg
PCR	< 1	ppm
Sulfated Ash	0.40	wt %
Ash	0.90	wt. %
Calorific Value cal/g	8070	cal/gram
Calorific Value BTU/lb	14526	BTU/lb
Total Sulfur	0.26	wt. %
Flash Point	221	degrees F
Total Halogens (Chlorine)	1120	ug/g

Approved by:

Craig Paul



LABORATORIES, Inc.

P.O. BOX 1873, 1411 S. 12th STREET
BISMARCK, ND 58502
PHONE (701) 258-9720 WATS (800) 279-6885 FAX (701) 258-9724



WE ARE AN EQUAL OPPORTUNITY EMPLOYER

FINAL ANALYSIS REPORT

Sample Number: 93-080

Report Date: 10/ 1/93

Mary Jo Connelly
PACE, Incorporated
1710 Douglas Drive North
Minneapolis, MN 55422

Work Order #: 31-0558
PO #: Pace#930909.505

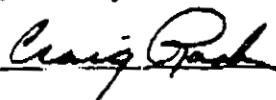
Date Received: 9/14/93

Sample Description: Oil Sample
Sample Site: #22979.2
Sample Location: Commercial Asphalt Company

Collection Date: 9/ 8/93

Analyte	Results	Units
pH	6.6	units
Lead Waste Oil	53.7	mg/kg
PCB	< 1	ppm
Sulfated Ash	0.35	wt %
Ash	0.84	wt. %
Calorific Value cal/g	10291	cal/gram
Calorific Value BTU/lb	18524	BTU/lb
Total Sulfur	0.41	wt. %
Flash Point	225	degrees F
Total Halogens (Chlorine)	987	ug/g

Approved by:





LABORATORIES, Inc.

P.O. BOX 1873, 1411 S. 12th STREET
BISMARCK, ND 58502
PHONE (701) 258-9720 WATS (800) 279-6885 FAX (701) 258-9724



WE ARE AN EQUAL OPPORTUNITY EMPLOYER

FINAL ANALYSIS REPORT

Sample Number: 93-081

Report Date: 10/ 1/93

Mary Jo Connelly
PACE, Incorporated
1710 Douglas Drive North
Minneapolis, MN 55422

Work Order #: 81-0558
PO #: Pace#930909.505

Date Received: 9/14/93

Sample Description: Oil Sample
Sample Site: #22980.6
Sample Location: Commercial Asphalt Company

Collection Date: 9/ 8/93

Analyte	Results	Units
pH	6.5	units
Lead Waste Oil	54.5	mg/kg
PCB	< 1	ppm
Sulfated Ash	0.39	wt %
Ash	0.81	wt. %
Calorific Value cal/g	10420	cal/gram
Calorific Value BTU/lb	18756	BTU/lb
Total Sulfur	0.51	wt. %
Flash Point	248	degrees F
Total Halogens (Chlorine)	965	ug/g

Approved by:



**LABORATO**P.O. BOX 249, 1128 N. FROM
NEW ULM, MN 56073-0249
PHONE (507) 354-8517 WAT**WE ARE AN EQUAL OPPORTUNITY EMPLOYER**

Post-It brand fax transmittal memo 7671

of pages 1

To	From
Co.	Co.
Dept.	Phone #
Fax #	Fax #

LIQUID ANALYSIS REPORTMARY JO CONNELLY
PACE LABORATORIES INC
1710 DOUGLAS DR N
MINNEAPOLIS MN 55422Date Reported: 10/27/93
Work Order #: 81-0558
Client Account Number: 007054

Project Name: 930909.505

Kim D. Sjogren, Lab Manager

Jeff Olson, ChemistNQ = Not Present, Qualitative Only
PQ = Present, Qualitative Only
BDL = Below Detection Limits
MDL = Method Detection Limits
ND = Not Determined**Test Methods**

VOC's - EPA Method 8021, MDH 465C



LABORATORIES, Inc.

P.O. BOX 249, 1128 N. FRONT STREET

NEW ULM, MN 56073-0249

PHONE (507) 354-8517 WATS (800) 782-3557 FAX (507) 359-2890

WE ARE AN EQUAL OPPORTUNITY EMPLOYER



Lab Number: 93-R359

Date Reported: 10/27/93

Work Order #: 81-0558

Date Sampled: 9/ 8/93

Client: PACE LABORATORIES INC

Date Received: 10/15/93

Temperature at Receipt: 5 C

EPA Method 8021

VOC Date Analyzed: 10/25/93

Sample Description: 079 (22978.4)

VOC Dilution Factor: 2.5

VOLATILE ORGANICS

Result.

Units

MDL

=====

=====

=====

=====

Chloroethane
 Chloromethane
 Bromomethane
 Dichlorodifluoromethane
 Vinyl Chloride
 Methylene Chloride
 Trichlorofluoromethane
 1,1-Dichloroethylene
 1,1-Dichloroethane
 trans-1,2-Dichloroethylene
 Chloroform
 1,2-Dichloroethane
 1,1,1-Trichloroethane
 Carbon Tetrachloride
 Bromodichloromethane
 1,2-Dichloropropane
 trans-1,3-Dichloropropane
 1,1,2-Trichloroethylene
 Chlorodibromomethane
 1,1,2-Trichloroethane
 cis-1,3-Dichloropropane
 2-Chloroethylvinyl Ether
 Bromoform
 1,1,2,2-Tetrachloroethane
 Tetrachloroethylene

BDL	ppm	5.0
BDL	ppm	5.0
BDL	ppm	5.0
BDL	ppm	5.0
BDL	ppm	1.3
BDL	ppm	3.5
BDL	ppm	4.8
8.3	ppm	3.3
BDL	ppm	0.5
BDL	ppm	0.8
BDL	ppm	2.5
BDL	ppm	1.5
44.3	ppm	2.8
BDL	ppm	1.0
BDL	ppm	1.8
BDL	ppm	1.0
BDL	ppm	0.8
2.6	ppm	1.0
BDL	ppm	1.0
BDL	ppm	0.8
BDL	ppm	1.3
NQ	ppm	ND
BDL	ppm	1.3
BDL	ppm	1.5
24.9	ppm	1.0



LABORATORIES, Inc.

P.O. BOX 249, 1126 N. FRONT STREET

NEW ULM, MN 56073-0249

PHONE (507) 354-8517 WATS (800) 782-3557 FAX (507) 359-2890

WE ARE AN EQUAL OPPORTUNITY EMPLOYER



Lab Number: 93-R359

Date Reported: 10/27/93

Work Order #: 81-0558

Date Sampled: 9/ 8/93

Client: PACE LABORATORIES INC

Date Received: 10/15/93

Temperature at Receipt: 5 C

EPA Method 8021

VOC Date Analyzed: 10/25/93

Sample Description: 079 (22978.4)

VOC Dilution Factor: 2.5

VOILATILE ORGANICS Halogens = -

=====	Result	Units	MDL
=====	=====	=====	=====
Chlorobenzene	BDL	ppm	0.8
-Benzene	27.7	ppm	5.0
Toluene	199.0	ppm	5.0
-Ethyl Benzene	66.2	ppm	3.8
1,2-Dichlorobenzene	BDL	ppm	1.5
1,3-Dichlorobenzene	BDL	ppm	1.0
1,4-Dichlorobenzene	BDL	ppm	0.5
cis-1,2-Dichloroethylene	BDL	ppm	2.0
1,3-Dichloropropane	BDL	ppm	1.5
1,2,3-Trichloropropane	BDL	ppm	1.8
Allyl Chloride	BDL	ppm	1.3
1,2-Dibromoethane	BDL	ppm	2.5
Methyl Ethyl Ketone	BDL	ppm	50.0
Methyl Isobutyl Ketone	BDL	ppm	3.8
Tetrahydrofuran	BDL	ppm	38.0
-m-Xylene & p-Xylene	248.0	ppm	5.0
o-Xylene	118.0	ppm	2.5
Cumene	BDL	ppm	3.8
1,1,1,2-Tetrachloroethane	BDL	ppm	1.3
1,1-Dichloro-1-propene	BDL	ppm	2.5
2,3-Dichloro-1-propene	BDL	ppm	2.5
Dichlorofluoromethane	NQ	ppm	ND
1,1,2-Trichlorotrifluoroethane 15.	-21.6	ppm	2.3
Ethyl Ether	BDL	ppm	7.5
Acetone	BDL	ppm	65.0
Dibromomethane	BDL	ppm	2.5
Pentachloroethane	NQ	ppm	ND
Dichloroacetonitrile	NQ	ppm	ND

**LABORATORIES, Inc.**

P.O. BOX 1873
1411 SOUTH 12TH STREET
BISMARCK, NORTH DAKOTA 58504
PHONE (701) 258-9720 FAX (701) 258-9724



November 15, 1993

Mary Jo Connelly
PACE, Incorporated
1710 Douglas Drive North
Minneapolis, MN 55422

RE: Total Halogens as Chlorine Results for Commercial Asphalt
Company.

Pace Sample ID#	MVTL Sample ID#	Initial Result	Rerun Result
#22978.4	93-079	1122 ug/g	870 ug/g
#22979.2	93-080	987 ug/g	1043 ug/g
#22980.6	93-081	965 ug/g	690 ug/g
	081 Duplicate		835 ug/g

If you have any questions please call our office at 701/258-9720.

Sincerely,

Rod Reetz
Laboratory Manager

APPENDIX C
Calculation Equations and Report Nomenclature

Calculation Equations

EPA Method 3 Calculations

Dry Molecular Weight of Flue Gas

$$M_d = (0.44 \times \%CO_2) + (0.32 \times \%O_2) + (0.28 \times (\%N_2 + \%CO))$$

Wet Molecular Weight of Flue Gas

$$M_s = M_d \times (1 - B_{ws}) + (18 \times B_{ws})$$

Percent Excess Air

$$\%EA = 100 \times \left(\frac{\%O_2 - (0.05 \times \%CO)}{(0.264 \times \%N_2) - \%O_2 + (0.5 \times \%CO)} \right)$$

Fuel F-factor (for comparison)

$$F_o = \frac{20.9 - \%O_2}{\%CO_2}$$

Where:

- B_{ws} = Water vapor in gas stream (proportion by volume).
- $\%CO$ = Carbon monoxide in gas stream (percent).
- $\%CO_2$ = Carbon dioxide in gas stream (percent).
- $\%EA$ = Excess air for combustion (percent).
- F_o = Fuel F-factor for results comparison.
- M_d = Molecular weight of dry flue gas (LB/LB-mole).
- M_s = Molecular weight of wet flue gas (LB/LB-mole).
- $\%N_2$ = Nitrogen in gas stream (percent).
- $\%O_2$ = Oxygen in gas stream (percent).

Calculation Equations

EPA Method 3 Calculations

Dry Molecular Weight of Flue Gas

$$M_d = (0.44 \times \%CO_2) + (0.32 \times \%O_2) + (0.28 \times (\%N_2 + \%CO))$$

Wet Molecular Weight of Flue Gas

$$M_s = M_d \times (1 - B_{ws}) + (18 \times B_{ws})$$

Percent Excess Air

$$\%EA = 100 \times \left(\frac{\%O_2 - (0.05 \times \%CO)}{(0.264 \times \%N_2) - \%O_2 + (0.5 \times \%CO)} \right)$$

Fuel F-factor (for comparison)

$$F_o = \frac{20.9 - \%O_2}{\%CO_2}$$

Where:

- B_{ws} = Water vapor in gas stream (proportion by volume).
- $\%CO$ = Carbon monoxide in gas stream (percent).
- $\%CO_2$ = Carbon dioxide in gas stream (percent).
- $\%EA$ = Excess air for combustion (percent).
- F_o = Fuel F-factor for results comparison.
- M_d = Molecular weight of dry flue gas (LB/LB-mole).
- M_s = Molecular weight of wet flue gas (LB/LB-mole).
- $\%N_2$ = Nitrogen in gas stream (percent).
- $\%O_2$ = Oxygen in gas stream (percent).

Calculation Equations

EPA Method 5 Calculations

Sample Volume, Standard Conditions

$$V_{std} = 17.647 \times V_m \times Y \times \left(\frac{P_b + \frac{\Delta H}{13.6}}{\bar{T}_m} \right)$$

Isokinetic Variation

$$I = 0.09450 \times \left(\frac{\bar{T}_s \times V_m}{P_s \times V_s \times A_n \times \theta \times (1 - B_{ws})} \right)$$

Particulate Concentration

$$C_s = 15.432 \times \left(\frac{m_n}{V_{std}} \right)$$

Particulate Mass Rate

$$m_p = 0.008571 \times C_s \times Q_{sd}$$

Where:

- A_n = Cross-sectional area of nozzle opening (square feet).
- B_{ws} = Water vapor in gas stream (proportion by volume).
- C_s = Particulate concentration of gas stream (GR/DSCF).
- ΔH = Orifice meter differential pressure (Inches WC).
- I = Isokinetic variation of sampling rate (percent).
- m_n = Total particulate collected in sampling train (grams).
- m_p = Particulate mass flow rate (LB/HR).
- P_b = Barometric pressure (Inches Hg).
- P_s = Absolute gas pressure of duct (Inches Hg).
- Q_{sd} = Dry standard volumetric gas flow rate (DSCFM).
- $\bar{T}_m$ = Sampling train meter temperature (°R).
- $\bar{T}_s$ = Flue gas temperature (°R).
- V_m = Volume of gas sample measured by gas meter (CF).
- V_{std} = Gas volume corrected to standard conditions (DSCF).
- V_s = Flue gas linear velocity (feet per second).
- Y = Dry gas meter calibration coefficient.
- θ = Total sampling time of run (minutes).

Calculation Equations

Nomenclature

A	= Cross-sectional area of duct
A_n	= Cross-sectional area of nozzle
B_{ws}	= Water vapor in gas stream, proportion by volume
C_a	= Particulate concentration, actual, wet basis - GR/ACF
C_p	= Pitot tube calibration coefficient
C_s	= Particulate concentration at dry standard conditions - GR/DSCF
%EA	= Excess air, percent by volume
F_o	= Fuel factor
G_d	= Specific gravity relative to air, dimensionless
I	= Isokinetic variation, percent by volume
M_d	= Molecular weight of flue gas, dry, lb/lb-mole
m_g	= Mass flow of wet flue gas, LB/HR
m_n	= Total particulate collected, grams
m_p	= Particulate mass flow, LB/HR
M_s	= Molecular weight of flue gas, wet, lb/lb-mole
P_b	= Barometric pressure, uncompensated, inches of mercury
P_g	= Static pressure of duct, inches of water
P_s	= Absolute gas pressure of duct, inches of mercury
Q	= Actual flue gas volumetric flow rate, ACFM
Q_{sd}	= Dry flue gas volumetric flow rate corrected to standard conditions, DSCFM
$\overline{T_m}$	= Average dry gas meter temperature, °R
$\overline{T_s}$	= Average stack gas temperature, °R
$\emptyset$	= Total sampling time, minutes
V_{lc}	= Total volume of liquid collected in impingers and desiccant, ml
V_m	= Volume of gas sample measured by gas meter, cubic feet
V_{std}	= Volume of gas sample corrected to standard conditions, dry standard cubic feet
V_w	= Volume of water vapor in gas sample, corrected to standard conditions
V_s	= Linear velocity of flue gas, feet per second
Y	= Dry gas meter calibration factor
ΔH	= Orifice meter differential pressure, inches of water
ΔP	= Velocity pressure of flue gas, inches of water
ρ	= Actual gas density, pounds per cubic foot

APPENDIX D
Test Procedures

OXYGEN AND CARBON DIOXIDE CONCENTRATION (ORSAT)

Integrated gas samples are collected in 40 liter Tedlar™ bags and ultimately transferred to an Orsat gas analyzer for oxygen and carbon dioxide analyses. A PACE sampling train which meets or exceeds the specifications of EPA Method 3, 40 CFR 60, Appendix A is used to collect gas samples. Normally, gas samples are collected at the exhaust of an EPA Method 4 or 5 sampling train since this gas stream is moisture conditioned. Method 4 and 5 sampling equipment is maintained and checked to assure no leaks occur between the flue and the integrated gas sampler.

Gas samples are collected by drawing a portion of the stream through a chemically resistant diaphragm pump and delivering it to the Tedlar™ bag at a constant, settable rate depending on expected sampling time. At the conclusion of sampling, the bag and associated hardware is sealed and labeled. When multiple tests are to be performed, gas samples are often transferred to glass gas collection tubes for storage. A portable oxygen analyzer is used for this to ensure sample integrity.

Samples are analyzed by chemical absorption using an Orsat gas analyzer. Following positive and negative leak checks of the gas analyzer, the system is purged with the gas to be analyzed. The buret is filled with approximately 100 mls of sample gas and the exact volume recorded. The sample line stopcock is closed and the stopcock for the first bubbler containing carbon dioxide absorbent is opened. Several passes are made, bubbling the sample gas through the reagent and the absorbent is returned to the initial mark. The new volume of the buret is recorded and an additional 1-2 passes are made to verify total absorption. Similar procedures are used to quantify oxygen with the same gas aliquot and oxygen absorbent.

PARTICULATE LOADINGS AND EMISSION RATES

Particulate emission rates were determined in accordance with EPA Methods 1-5, 40 CFR 60, Appendix A. Using traverse points determined with EPA Method 1, a preliminary velocity profile was obtained with respect to the velocity traverse, gas temperature, gas pressure and estimated moisture content. From this data sampling nozzles of the appropriate diameter to ensure isokinetic sampling were selected.

The particulate sampling train consists of a temperature controlled glass-lined sampling probe equipped with a S-type pitot tube and Type K thermocouples to monitor stack temperature and probe liner temperature. The sampling probe is attached to a sample module which houses an all glass in-line filter and cyclone assembly in a temperature controlled oven. The back half of the sampling train consists of a series of three glass impingers followed by a tared desiccant-packed drying column. The sample train is connected by means of a control and sampling umbilical cord to the control module. The control module houses a temperature monitored dry test gas meter, a calibrated orifice, dual inclined manometers, temperature controllers, and necessary flow rate control devices.

Particulate samples are collected by isokinetically extracting a sample gas stream from the flue by means of the sampling probe and passing the stream through the cyclone which collects larger, heavier particles. The sample gas stream then passes through a 4 inch diameter Gelman Type A/E glass fiber filter to collect finer particulates. The filter is followed by an ice-cooled impinger train and a desiccant packed drying column which quantitatively collects all moisture from the sample gas stream. The gas then passes through a leak proof rotary vane sampling pump and a dry test gas meter which integrates the sample volume throughout the course of the test. A calibrated orifice is connected to the gas meter outlet to facilitate sample flow rate adjustment.

Representative particulate samples are collected by sampling the centroid of equal area sections of the duct for equal time periods. The sampling rate is adjusted at each traverse point to ensure isokinetic sampling. Pre-programmed

field computers are used to facilitate rapid determination of the correct sampling rate.

Integrated gas samples are collected concurrently with particulate samples to determine a representative gas composition of the flue gas. Gas samples are collected in Tedlar™ bags throughout the course of the particulate run and analyzed with an Orsat gas analyzer.

At the end of each particulate run, the sampling train is disassembled and the samples recovered. The sampling filter is transferred from the filter holder to its dedicated petri dish. The probe nozzle is acetone rinsed, brushed, rinsed again and the washings placed in a uniquely labeled polyethylene container. The probe is similarly cleaned; acetone rinsed, brushed several times, rinsed again and the washing transferred to the same polyethylene container. The filter holder and cyclone are wiped free of silicone grease, acetone rinsed, brushed, rinsed and these washings added to the probe wash container. The container is tightly capped and the liquid level marked for transport. The impinger catch volume is determined to the nearest milliliter using a graduated cylinder. If the impinger catch is to be analyzed it is transferred to a separate polyethylene container, capped, and the liquid level marked. The desiccant-packed drying column is weighed in the field to the nearest 0.5 g and the weight of absorbed moisture added to the condensate for moisture calculations.

Particulate samples are transported back to the laboratory, logged in, and prepared for analyses. Filters are desiccated for 24 hours and weighed to a constant weight and the results recorded to the nearest 0.1 mg. Probe wash samples are evaporated at ambient temperatures to dryness in tared evaporating dishes. They are then desiccated for 24 hours and weighed to a constant weight. Results are reported to the nearest 0.1 mg.

WET CATCH ANALYSIS - ORGANIC CONDENSIBLES

Particulate concentrations reported in this document include gravimetric results of both the dry catch and the organic wet catch. Organic condensibles were collected in a series of three ice-cooled all-glass impingers in the back half of the Method 5 sampling train. The first two impingers were initially prepared with 100 mls of deionized water in each and the third impinger was dry. After sampling, the volume of condensate in the impingers was determined and the contents transferred to an air-tight polyethylene sample container.

The wet catch was analyzed for condensible organic particulate with the chloroform/diethyl ether extraction. Three 25 ml portions of chloroform and three 25 ml portions of diethyl ether were used to extract condensed organics from the impinger catches (wet catch). The extractions were evaporated at room temperature and desiccated to a constant weight. Gravimetric results were then added to dry catch results to calculate particulate concentrations.

APPENDIX E
Quality Assurance Data

Commercial Asphalt Company
Ramsey, Minnesota
PACE Project No. 930831.401

PACE Incorporated
September 17, 1993

Air Sampling Department Calibration Report

Sampling Nozzle Calibration Data

Nozzle Number : 2-3
Date of Calibration : 9/3/93
Calibration Technician: T. Kuchinski

Measurement Position	Diameter Inches
1	0.310
2	0.312
3	0.310
4	0.311
5	0.312
Average	0.311

The sampling nozzle is rotated and measured at 36 degree
Increments. Diameters are measured to the nearest 0.001".
All measurements must be within a range of 0.004".

Commercial Asphalt Company
Ramsey, Minnesota
PACE Project No. 930831.401

PACE Incorporated
September 17, 1993

Air Sampling Department Calibration Report

Pitot Tube Calibration Data

Pitot Tube Number : 8
Date of Calibration : 6/7/93
Calibration Technician: K. Lattery

A Side Calibration

Calibration Trial No.	ΔP (standard) Inches WC	ΔP (S-type) Inches WC	Pitot Coefficient
1	0.500	0.700	0.837
2	0.805	1.120	0.839
3	1.085	1.515	0.838
4	1.305	1.805	0.842
A Side Average			0.839

B Side Calibration

Calibration Trial No.	ΔP (standard) Inches WC	ΔP (S-type) Inches WC	Pitot Coefficient
1	0.505	0.700	0.841
2	0.820	1.130	0.843
3	1.100	1.530	0.839
4	1.300	1.805	0.840
B Side Average			0.841
Pitot Tube Coefficient			0.840

Commercial Asphalt Company
 Ramsey, Minnesota
 PACE Project No. 930831.401

PACE Incorporated
 September 17, 1993

Air Sampling Section Calibration Report

Dry Test Meter and Orifice Calibration Data

Control Module Number : C-6 Calibration Technician: M.Wilson

Date of Calibration : 9/3/93 Barometric Pressure : 29.08

Orifice Diff. Press., ΔH Inches WC	Dry Test Meter Vol. Cubic Ft.	Wet Test Meter Vol. Cubic Ft.	Dry Test Meter Temperatures, °F		Wet Test Meter Temp., °F	Elapsed Time Minutes	Gas Meter Coefficient <u>_____</u>	Orifice Coefficient ΔH@ <u>_____</u>
			Inlet	Outlet				
0.50	5.090	5.000	88.0	78.0	73.0	13.343	0.9995	2.031
1.00	5.070	5.000	88.0	76.0	73.5	9.545	0.9994	2.086
1.75	5.050	5.000	83.5	73.5	73.5	7.276	0.9950	2.135
2.50	10.100	10.000	87.5	74.5	73.5	12.324	0.9977	2.178
3.50	10.160	10.000	89.5	79.0	73.5	10.403	0.9953	2.159

Average Meter Coefficient 0.9974

Average Orifice Coefficient 2.118

APPENDIX F
Process/Source Information

MPCA EXHIBIT C

SOURCE OPERATIONAL DATA

Rev/YH/93

9-8-73

Type (circle one): Drum Mix Conventional
Other (list): _____

Pollution Control Equipment: Baghouse Venturi Scrubber wet scrubber cyclone multiclone
 (circle one)
 List model: CMI SUM-12 If wet scrubbing: _____ % scrubber water recycled
 Air flow through control equipment: 80,000 acfm at _____ F Normal pressure drop across control equipment: 5.2 inches water
 Date & procedures of last maintenance/cleaning of control equipment: 8-30-73 Was control equipment operating normally during testing? yes
Darklight & changed filter Dust Blower

temize all fuels and materials added to the combustion process during the test period. List fuel type used during testing (if oil, specify grade) _____. If other units of measure are used, specify and calculate appropriate heat input.

Test No. ____	Fuel Input (Gal/hr)	BTU/GAL (as received)	Heat Input (BTU/HR)	%Moisture (as received in aggregate)		
				Virgin	recycle	combined
Run 1	780					
Run 2	760					
Run 3	780					

is the above fuel substantially the highest sulfur containing fuel normally burned? YES
 Production specific fuel usage: (circle one) measured _____ or calculated: _____ cubic foot/ ton hot mix
 _____ gal/ton hot mix
 No. of Burners: ONE Burner(s) rating: 175 MMBTU/HR = 100% setting
 Add for TOTAL AGG TPN.

[illegible]

Plant Operator's Certification: I certify that the information submitted herein is accurate and correct and that no information requested was withheld from the Division Manager.

By: T/ev Nesoi, Phone: () 431-0832

Position: _____

Note: All information required must be completed and submitted as part of the performance test. Failure to submit the required information will result in an incomplete performance test report.

Generation:

Test Date(s):

[illegible]

567.8
 579.4
 571.3
 579.5
 582.5
 574.4

 575.82

$$\begin{array}{r} 570 \\ 574.7 \\ 572.8 \\ 576.2 \\ 565.8 \\ 571.1 \\ \hline 571.77 \end{array}$$

Plant Operator's Certification: I certify that the information submitted herein is accurate and correct and that no information requested was withheld from the Division Manager.

By: Walter Nelson Phone: (421) 0832

Position: _____

Note: All information required must be completed and submitted as part of the performance test. Failure to submit the required information will result in an incomplete performance test report.

DATE
09/08/1993

TIME
07:35

MIX# , SILO
12 2

***** AUTOMATIC *****

ATERIAL	MIX PERCENT	TARGET	ACTUAL	TONS	PERCENT MOISTURE
GG 1	32.5	187.2	187.2	00192.08	5.5
AGG 2	32.5	187.2	187.2	00192.08	5.0
GG 3	5.0	28.8	28.8	00027.05	5.0
GG 4	0.0	0.0	0.0	00000.00	5.0
AGG 5	0.0	0.0	0.0	00005.11	5.0
AGG 6	0.0	0.0	0.0	00000.00	5.0
/C	5.5	23.40	23.49	00022.690	
ILLER	0.0	0.00	0.00	00000.000	
RECYCLE 1	30.0	172.8	172.8	000160.52	5.0
ESIDUAL A/C	5.0				
ECYCLE 2	0.0	0.0	0.0	000000.00	0.0

ECYCLE SCALE	186.3	000164.89	5.0
AGG SCALE	385.6	000387.52	5.2

VERAGE A/C CONTENT	4.03 NEW	5.48 TOTAL
EALTIME A/C CONTENT	5.51	

MIX TEMP. = 254 F
/C TEMP. = 256 F

EXHAUST TEMP. = 244 F
OUTLET = 235 F

BURNER FUEL VALVE = 065 PERCENT

DATE
09/08/1993

TIME
13:07

MIX# SILO
12 2

***** AUTOMATIC *****

MATERIAL	MIX PERCENT	TARGET	ACTUAL	TONS	PERCENT MOISTURE
AGG 1	32.5	186.9	186.9	00817.19	5.5
AGG 2	32.5	186.9	186.9	00817.19	5.0
AGG 3	5.0	28.8	28.8	00156.09	5.0
AGG 4	0.0	0.0	0.0	00014.60	5.0
AGG 5	0.0	0.0	0.0	00005.11	5.0
AGG 6	0.0	0.0	0.0	00057.34	5.0
A/C	5.5	23.59	23.39	00106.513	
FILLER	0.0	0.00	0.00	00000.000	
RECYCLE 1	30.0	172.5	172.5	000781.06	5.0
RESIDUAL A/C	5.0				
RECYCLE 2	0.0	0.0	0.0	000000.00	0.0

RECYCLE SCALE	167.4	000786.09	5.0
AGG SCALE	387.3	001755.08	5.2

AVERAGE A/C CONTENT 4.20 NEW 5.70 TOTAL
REALTIME A/C CONTENT 5.47

MIX TEMP. = 276 F EXHAUST TEMP. = 270 F BURNER FUEL VALVE = 070 PERCENT
A/C TEMP. = 263 F OUTLET = 250 F

DATE
09/08/1993

TIME
16:07

MIX# SILO
12 2

***** AUTOMATIC *****

MATERIAL	MIX PERCENT	TARGET	ACTUAL	TONS	PERCENT MOISTURE
AGG 1	32.5	187.2	187.2	01297.36	5.5
AGG 2	32.5	187.2	187.2	01297.36	5.0
AGG 3	5.0	28.8	28.8	00279.46	5.0
AGG 4	0.0	0.0	0.0	00036.64	5.0
AGG 5	0.0	0.0	0.0	00005.11	5.0
AGG 6	0.0	0.0	0.0	00122.00	5.0
A/C	5.5	23.10	23.30	00175.670	
FILLER	0.0	0.00	0.00	00000.000	
RECYCLE 1	30.0	172.8	172.8	001283.73	5.0
RESIDUAL A/C	5.0				
RECYCLE 2	0.0	0.0	0.0	000000.00	0.0

RECYCLE SCALE	172.5	001288.39	5.0
AGG SCALE	383.9	002862.67	5.2

AVERAGE A/C CONTENT	4.14 NEW	5.64 TOTAL
REALTIME A/C CONTENT	5.54	

MAY TEMP. = 278 F	EXHAUST TEMP. = 271 F	BURNER FUEL VALVE = 070 PERCENT
A/C TEMP. = 272 F	OUTLET = 250 F	

Commercial Asphalt Company
Ramsey, Minnesota
PACE Project No. 930831.401

PACE Incorporated
September 15, 1993

APPENDIX C
METHOD 5 CALCULATION SUMMARY
TEST 1

Baghouse Outlet

Parameter	Run 1	Run 3	Run 4
Date of Run	9/8/93	9/8/93	9/8/93
Sample Duration (Minutes)	60	60	60
Barometric Pressure (inches Hg)	29.16	29.16	29.16
Static Pressure Of Duct (Inches H2O)	0.22	0.22	0.22
Absolute Pressure Of Duct (Inches Hg)	29.18	29.18	29.18
Meter Coefficient	0.9974	0.9974	0.9974
Pitot Tube Coefficient	0.84	0.84	0.84
Nozzle Diameter (Inches)	0.311	0.311	0.311
Area Of Nozzle Opening (Square Feet)	0.000528	0.000528	0.000528
Average $\sqrt{\Delta P}$	0.7223	0.6833	0.6847
Average ΔH	2.36	2.06	2.16
Average Stack Temperature (°R)	682.35	701.40	702.30
Average Meter Temperature (°R)	530.78	553.18	552.23
Meter Volume (Cubic Feet)	48.19	45.9	47.06
Dry Standard Sample Volume (Cubic Feet)	46.88	42.81	43.98
Collected Condensate Volume (mls)	520.0	460.0	500.0
Volume Of Water Vapor (Standard Cubic Feet)	24.48	21.65	23.54
Moisture Content Of Flue Gas (% v/v)	34.30	33.59	34.86
Weight Of Particulate (mg)	63.4	55.4	53.8
Particulate Concentration (GR/DSCF)	0.02085847	0.01998584	0.01888968
Source Gas Velocity (Feet Per Second)	49.6	47.4	47.7
Isokinetic Variation (%)	100.5	97.6	101.7

REQUIRED DATA
for
COMBUSTION SOURCES

Company Name Commercial Asphalt

C. Fuel Input

1. Itemize all fuels and materials that are added to the combustion process during the test period. Attach ultimate analysis of the fuel.

FUEL DESCRIPTION Coal: State, City, Mine Oil: Specify Grade	INPUT (LBS/HR) (GAL/HR)	& MOISTURE As Rec'd	As Rec'd (BTU/LB) (BTU/GAL)	HEAT INPUT (BTU/HR)
No. 1 <u>USED</u>	<u>780</u>			
No. 2 <u>Used</u>	<u>760</u>			
No. 3 <u>USED</u>	<u>780</u>			

TOTAL _____

2. Are the above fuels substantially the same as those normally burned?

Yes. If not, explain _____

3. Are the above fuels normally burned in the proportions shown above?

Yes. If not, explain _____

4. Describe any changes anticipated for procurement of fuels within the next twelve (12) months.

None

D. Equipment & Operating Data

1. Furnace No. Plant #6

2. Furnace Mfg. Hauck

3. Type of Firing _____

4. Furnace operating under normal operating conditions: No _____;

Yes

4. Submittal Schedule

Performance test reports shall be submitted no later than 45 days following completion of the performance test, or as required in compliance document (permit, stipulation agreement, Administrative Penalty Order, etc.), the Supervisor, CDU within 45 days of testing.

The Permittee is also responsible for providing a microfiche copy of the Performance test report within 105 days of testing. To microfiche a copy of a performance test report, contact the State Department of Administration-Micrographics Services Unit at (612)296-9708. The complete permit file number, complete facility name, and the exact date of testing must be provided.

5. Specify normal soot blowing frequency:

a) source operating time blowing soot: _____ minutes/shift

b) number of shifts per day _____

6. Specify soot blowing time during the test: start _____ end _____.
When was the last time before the test that you blew soot: (date & time)
_____.

7. Specify normal ash pulling frequency:

a) source operating time pulling ashes: _____ minutes/shift

b) number of shifts per day _____

8. Specify ash pulling time during the test: start _____ end _____.
When was the last time before the test that you pulled ashes: (date & time)
_____.

9. Date and procedures of last maintenance/cleaning of the boiler (please attach) _____.

E. Instrument Data

1. Include a copy of chart records during test for the combustion efficiency indices (CO, O₂, CO₂, combustibles, steam flow, air flow, etc.)

F. Air Pollution Control Equipment

1. Type/model control equipment Baghouse CMT SAF 720 SUM-12

2. Air pressure drop across the control equipment 5.3

3. Air flow through the control equipment 80000 ACFM

4. Was the control equipment operating normally? yes

5. Date and procedures of last maintenance/cleaning of control equipment.

8-30-93 Backlighted & changed
Dust Blower Filter

Plant Operator's Certification

I certify that the information submitted herein is accurate and correct and that no information requested was withheld from the Division Manager.

By [Signature], Position Plant Operator

REQUIRED DATA
for
PROCESS EMISSIONS

Company Name Commercial Asphalt

C. Equipment & Operating Data

1. Process Equipment No./Ident. _____
2. Process Equipment Description Baghouse
3. Process equipment operating under normal operating conditions?
No ____ Yes (circled) ____ Process rate during the test 580
(raw materials or finished product)

D. Instrument Data on Process Equipment

1. Include copy of production records or instrumentation which indicates rate of production or operation of the equipment, i.e. units per hour, lbs. per hour, pressure, air flow, etc.

E. Air Pollution Control Equipment

1. Type/model of control equipment CMT Baghouse SVM-12
2. Air pressure drop across the control equipment 5.2
3. Air flow through the control equipment 80 000 ACFM
4. Was the control equipment operating normally? Yes
5. Data of last major maintenance/cleaning of control equipment
8-30-93 Blower & changed dust
Blower Filter

F. Plant Manager's Certification

I certify that the information submitted herein is accurate and correct and that no information requested was withheld from the Division Manager.

By [Signature]

Position Plant Operator

lmb1770