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DIVISION OF ENVIRONMENTAL MANAGEMENT
AIR QUALITY SECTION

November 4, 1987

MEMORANDUM

TO: Ken Schuster

FROM: Robert Wooten 

SUBJECT: Review of Report of Particulate and Visible Emissions Testing
Performed on the Rotary Dryer Baghouse Stack at Cumberland
Paving Company, Princeton, Johnston County, North Carolina.

The tests were performed June 29, 1987 by personnel of Entropy Environmentalists. The report was received July 21, 1987 at the Raleigh Regional Office and some time later at the central office.

This asphalt plant is regulated under NSPS Subpart I.

EPA Method 9 was used to perform the visible emissions test. The observer was properly certified at the time of the test. It appears that correct procedures were followed. No visible emissions were recorded. Subpart I permits emissions of less than 20% opacity.

EPA Method 5 was used to determine particulate emissions. The only problem noted was that Run 1 was 84.8% isokinetic whereas 90% is the acceptable lower limit. The likely result of this is that the reported emissions of Run 1 are somewhat greater than the actual emissions. The average emission concentration of the three runs was .0108 grains per DSCF whereas Subpart I allows up to .04 grains per DSCF. Compliance is well demonstrated.

/lhb

cc: Mike Aldridge
Central File

NORTH CAROLINA DIVISION OF ENVIRONMENTAL MANAGEMENT

Air Quality Action Request

Computer _____

Name	Location	Reg/Co./Prem. No.
CUMBERLAND PAVING	SR 1002, Princeton	5/51(Johnston)/0013
Contact	Telephone	
Bobby Narron, Hugh Smith-foreman	936-4411	
Type Action:	CI ☐ EE ☒ SR ☐ PC ☐ VE ☐ PI ☐ Other ☐	NSPS
		stack test
Air Program Status	03 92	Class AIP Chg
Action Requested By:	Address/Phone	Rec'd Date
Last Insp. Date	Action Date	Next Insp. Date
00-00-00	6/29/87	6/30/88
Permit #	Issued	Expires
5447	5/22/84	4/1/89
Stip. #	Met Y/N	Y
Recommendations:	Signature	Date
	David Daniel 	7/6/87
Dist: Yellow (Central File) - Blue (Region) - White (Opt.) Specify		

This plant is a drum mix asphalt plant. Emission points are controlled by a baghouse-6532 sq.ft. of filter area; Astec Super Six Pack.

At the time of the inspection, a stack test was being conducted. Attached is my AQ-92, for your convenience.

NSPS information:

The plant was operating at 300 tph (black base) while burning #2 fuel oil in the rotary dryer. No VEs were seen during the test.

1. first batch was produced 6/8/87
2. maximum production was reached 6/22/87
3. the plant stack tested for particulate and VE 6/29/87.

Await stack test results.

DYD/jf

**SOURCE TEST
OBSERVERS CHECKLIST**

N. C. Division of Environmental Management / Air Quality Section

Source Name: <u>Comberland Paving</u> Address: <u>Princeton</u> Plant Location: <u>Johnston Co.</u> Source Location: <u>S.R.1002</u> Contact: <u>Bobby Darron</u> Phone: <u>936 4411</u>	Testing Firm: <u>Entropy Envir.</u> Address: <u>RTP</u> Phone: _____ Test Engineer: <u>Tom McDonald</u> Assistant: <u>Mark Cuen</u>
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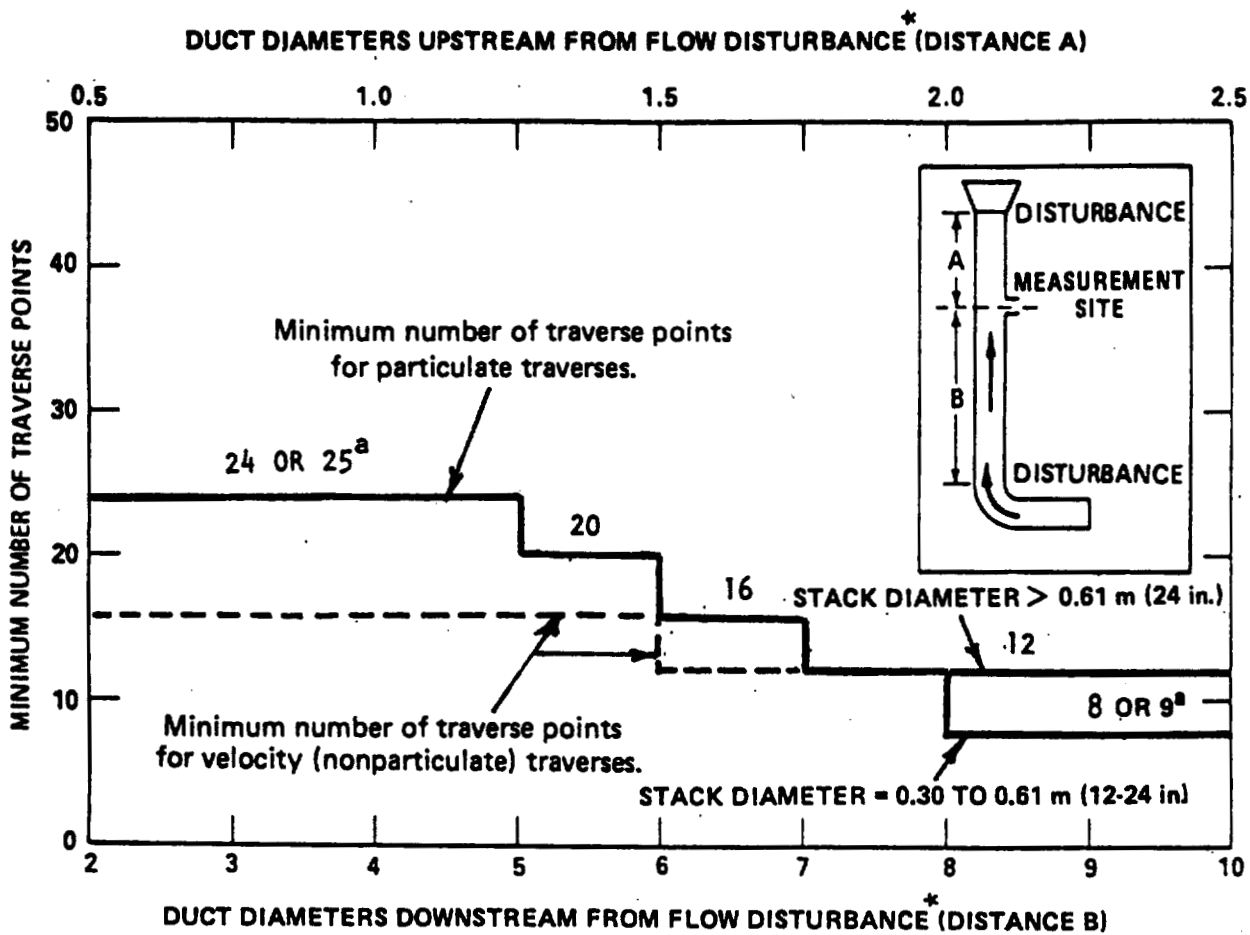
Other Personnel Involved	Affiliation
<u>Hugh Smith Foreman - Ptop.</u>	<u>CPC</u>
<u>Michael Kirkman</u>	<u>Entropy VEE</u>
<u>Wesley Wooten</u>	<u>D.O.T.</u>

Process Description: <u>Drum Mix</u> <u>300TPH Asphalt Plant</u> Process Rate _____ During Test: <u>300TPH Base</u> Maximum _____ Process Rate: <u>300TPH</u> Burner Sizes _____ (Incin) Pri: <u>NA</u> Sec: <u>NA</u>	Soot Blowing Parameters: A = <u>NA</u> Hr B = _____ Hr R = _____ Hr S = _____ Hr A = Hours of soot blowing during sample(s) B = Hours not soot blowing during sample(s) containing soot blowing R = Average hours of operation per 24 hours S = Average hours of soot blowing per 24 hours
---	--

TEST PARAMETERS	TEST PARAMETERS
Duct Size: <u>29 1/2" x 45"</u> Distance Before Ports: <u>87"</u> Distance After Ports: <u>19"</u> Number of Test Points: <u>24</u> Number of Runs: <u>3</u> Sampling Time Per Run (min.): <u>60</u>	Pollutant Sampled: <u>Particulate & VE</u> E. P. A. Method No.: <u>5 & 9</u> If method differs from E. P. A. method, explain: For Method 5 sampling train record ΔH_a <u>1.75</u> Y. <u>9974</u>

Leakage Rate (ft ³ /min.) (0.02 ft ³ /min. or less)	Run #1	Run #2	Run #3
	<u>.002/.000</u>	<u>.001</u>	<u>not blown</u>
Time Started	<u>9:49 AM</u>	<u>1:08 PM</u>	
Time Ended	<u>12:33 PM</u>		
Test Date(s)	<u>6-29-87</u>	<u>6-29-87</u>	<u>1 1</u>

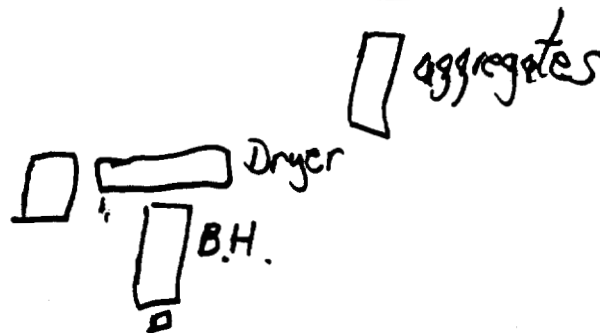
See Graph on Reverse Side For Number of Test Points. Use Reverse Side for Comments.	Request 2 Copies of Report <u>Ch. Daniel</u> OBSERVERS SIGNATURE <u>6-29-87</u>
---	---



^a HIGHER NUMBER IS FOR
RECTANGULAR STACKS OR DUCTS

COMMENTS;

SR 1002



paving lot. - next week.
calcium chloride.

○ Sun

CUMBERLAND PAVING
PRINCETON
ROTARY DRYER BAGHOUSE
29 JUNE 1987

	RUN NUMBER	1	2	3
Ms	WET MOLECULAR WT., #/#-MOLE	27.74	ERR	ERR
Pstatic	GAS STATIC PRESS., IN. H2O	-0.95		
Ps	ABSOLUTE GAS PRESS, IN. HG.	29.83	0.00	0.00
TsF	STACK GAS TEMP., DEG. F	279		
SSR DP	SUM OF SQUARE ROOTS OF VELOCITY PRESS. VALUES	30.1001		
vs	FLUE GAS VELOCITY, FT/SEC	85.1	ERR	ERR
Ds	DUCT DIAMETER, INCHES	29.5X45		
As	DUCT AREA, SQUARE INCHES	1327.5	0.0	0.0
AsF	DUCT AREA, SQUARE FEET	9.219	0.000	0.000
Qs	GAS FLOW RATE, WET ACFM	47071	ERR	ERR
Qstd	GAS FLOW RATE, DRY SCFM	29048	ERR	ERR
mri	SAMPLE WEIGHT, GRAMS	0.0277		
cs	PART. CONCENTRATION GR/DSCF	0.0138	ERR	ERR
pmrc	POLLUTANT MASS RATE CALC. FROM CONCENTRATION, #/HR	3.43	ERR	ERR
pmra	POLLUTANT MASS RATE CALC. FROM AREA RATIO, #/HR	2.92	ERR	ERR
%I	% ISOKINETIC	85.2	ERR	ERR
pmr avg	AVERAGE OF pmra & pmrc	3.17	ERR	ERR
%EA	% EXCESS AIR	235.0	ERR	ERR
F	"F" FACTOR, CU FT/MIL BTU			
o	HEAT INPUT RATE, MIL BTU/HR	ERR	ERR	ERR
e	EMISSION RATE, #/MIL BTU	ERR	ERR	ERR

CUMBERLAND PAVING
PRINCETON
ROTARY DRYER BAGHOUSE
29 JUNE 1987

	RUN NUMBER	1	2	3
	RUN DATE	29JUNE 87		
	RUN START TIME	9:49 AM		
	RUN FINISH TIME	12:33 PM		
N	NUMBER OF SAMPLE POINTS	24		
Theta	TEST RUN TIME, MINUTES	60		
Dr	NOZZLE DIAMETER, INCHES	0.188		
Ar	NOZZLE AREA, SQ. IN.	0.0278	0.0000	0.0000
Cp	PITOT TUBE COEFFICIENT	0.840		
Y	GAS METER CAL. FACTOR	0.997		
Pbar	BAROMETRIC PRESSURE, IN. HG	29.90		
Delta H	AVG. PRESS. DIFFERENTIAL OF ORIFICE METER, IN. H2O	0.983		
Vm	ACTUAL METERED GAS VOL. CF	32.757		
TmF	GAS METER TEMP., DEG. F	96		
Vm(std)	METERED GAS VOLUME AT DRY STANDARD CONDITIONS, DSCF	31.056	0.000	0.000
Vwc	VOLUME OF WATER COLLECTED IN IMPINGERS & DESICCANT, ML	101.5		
Vwc(std)	VOLUME OF WATER VAPOR, SCF	4.778	0.000	0.000
%M	MOISTURE, % BY VOLUME	13.3	ERR	ERR
fm	MOLE FRACTION OF DRY GAS	0.867	ERR	ERR
%CO2	CO2, % BY VOLUME, DRY	4.0		
%O2	O2, % BY VOLUME, DRY	15.0		
%CO	CO, % BY VOLUME, DRY	0.0		
%N2	N2, % BY VOLUME, DRY	81.0		
Md	DRY MOLECULAR WT., #/#-MOLE	29.24	0.00	0.00

SOURCE Cummins Engine Co.STATION/UNIT 11-0000

		1	2	3
	RUN DATE	2-2-77		
	RUN START TIME	5:41 PM		
	RUN FINISH TIME	5:53 PM		
N	NUMBER OF SAMPLE POINTS	24		
Theta	TEST RUN TIME, MINUTES	60		
Dn	NOZZLE DIAMETER, INCHES	.187		
Cp	PITOT TUBE COEFFICIENT	.84		
Y	GAS METER CAL. FACTOR	1.007		
Pbar	BAROMETRIC PRESSURE, IN. HG	29.9		
Delta H	AVG. PRESS. DIFFERENTIAL OF ORIFICE METER, IN. H2O			
Vm	ACTUAL METERED GAS VOL. CF	2.7		
TmF	GAS METER TEMP., DEG. F	56		
Vwc	VOLUME OF WATER COLLECTED IN IMPINGERS & DESICCANT, ML	101.5		
ZCO2	CO2, % BY VOLUME, DRY	4.5		
ZO2	O2, % BY VOLUME, DRY	15.5		
ZCO	CO, % BY VOLUME, DRY	0		
ZN2	N2, % BY VOLUME, DRY	80		
Pstatic	GAS STATIC PRESS., IN. H2O	-2.9		
TsF	STACK GAS TEMP., DEG. F	279		
SSR DP	SUM OF SQUARE ROOTS OF VELOCITY PRESS. VALUES	92.1		
Ds	DUCT DIAMETER, INCHES	20		
As	DUCT AREA, SQUARE INCHES	1327.5		
AsF	DUCT AREA, SQUARE FEET			
mn	SAMPLE WEIGHT, GRAMS	157		
F	"F" FACTOR, CU FT/MIL BTU			

DIVISION OF ENVIRONMENTAL MANAGEMENT
RALEIGH REGIONAL OFFICE

Date: Aug 17, 1987

M E M O R A N D U M

TO: Mike Aldridge

FROM: Kenneth Schuster/D. Daniel

SUBJECT: Request for Source Test Review

Company: Cumberland Paving, Princeton

County: Johnston

It is requested that the attached subject source test dated June 29, 1987
be reviewed. It is 1 of 1 copy(s).

Additional Comment:

arg Q - accept as is - 8-13-87

*The arg. emission (part.) rate of 0.011 g/dscf appears
to show compliance with the allowable rate of 0.04 g/dscf
Opacity appears to meet compliance also.*

KS:

Attachment

ENTROPY

ENVIRONMENTALISTS INC.

POST OFFICE BOX 12291
RESEARCH TRIANGLE PARK
NORTH CAROLINA 27709-2291
919-781-3550

RECEIVED

JUN 27

STATIONARY SOURCE SAMPLING REPORT
EEI REF. NO. 5569

RALEIGH REGIONAL OFFICE

CUMBERLAND PAVING COMPANY
CONTINUOUS MIX ASPHALT PLANT
PRINCETON, NORTH CAROLINA

PARTICULATE EMISSIONS AND PLUME OPACITY COMPLIANCE TESTING

ROTARY DRYER BAGHOUSE STACK

JUNE 29, 1987

REPORT CERTIFICATION

The sampling and analysis performed for this report was carried out under my direction and supervision.

Date July 14, 1987

Signature Arthur T. McDonald
Arthur T. McDonald

I have reviewed all testing details and results in this test report and hereby certify that the test report is authentic and accurate.

Date July 14, 1987

Signature D. James Grove
D. James Grove, P.E.

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INTRODUCTION

1.1 Outline of Test Program. Stationary source sampling was performed for Cumberland Paving Company at the continuous mix asphalt plant in Princeton, North Carolina on June 29, 1987. Three EPA Method 5 runs were performed at the rotary dryer baghouse stack to determine the particulate emissions. EPA Method 9 plume opacity determinations were conducted concurrently with the particulate emissions testing.

1.2 Test Participants. Table 1-1 lists the personnel present during the test program.

TABLE 1-1
TEST PARTICIPANTS

Cumberland Paving Company	Bobby Narron Test Coordinator
North Carolina Department of Natural Resources and Community Development	David Daniel Test Observer
Entropy Inc.	Arthur T. McDonald Project Supervisor
	Michael L. Kirkman Sampling Team Leader & Visible Emissions Observer
	Mark K. Owens Engineering Technician

SUMMARY OF RESULTS

2.1 Presentation. Table 2-1 summarizes the results of the particulate emissions testing performed June 30, 1987, at the baghouse stack. Detailed test results are given in Appendix A; field and analytical data are presented in Appendix B.

2.2 Discussion

2.2.1 Particulate Emissions. The average particulate concentration was 0.011 grains per dry standard cubic foot (gr/DSCF). The maximum concentration of particulate allowed by the United States EPA New Source Performance Standards for Asphalt Concrete Plants is 0.04 gr/DSCF.

2.2.2 Plume Opacity. All stack plume opacity readings were zero. Field data and observer certification documentation are given in Appendix B.2.

2.2.3 Run 1 Sampling Rate. Run 1 was performed at an isokinetic sampling rate which is slightly lower than the EPA minimum limit of 90%. Due to an overestimate of the moisture content while setting the sampling parameters, run 1 was performed with a sampling rate at 85% isokinetic.

Assuming worst case condition (all particles being greater than 50 microns in diameter), the maximum error would result in the measured concentration for run 1 being 15% higher than real. If the reported concentration for run 1 of 0.014 grains per dry standard cubic foot (gr/DSCF) is reduced for the worst case error, the adjusted concentration would be 0.012 gr/DSCF. The average concentration would decrease from 0.011 gr/DSCF to 0.010 gr/DSCF, a decrease of 10%.

TABLE 2-1
PARTICULATE TESTS SUMMARY OF RESULTS

Dryer Baghouse Stack

	1 ----	2 ----	3 ----
Run Date	6/29/87	6/29/87	6/29/87
<u>Test Train Parameters:</u>			
Volume of Dry Gas Sampled, SCF*	31.056	37.057	35.974
Percent Isokinetic	84.8	102.0	99.4
<u>Flue Gas Parameters:</u>			
Temperature, Degrees F	275	270	259
Volumetric Air Flow Rates SCFM*, Dry	29,162	28,920	28,818
ACFM, Wet	46,900	46,502	45,113
Excess Air, Percent	235.0	235.0	235.0
<u>Method 5 Results:</u>			
Catch, Milligrams	27.7	25.8	18.3
Concentration, Grains/DSCF*	0.01376	0.01074	0.007850
Emission Rate, Lbs/Hour	3.441	2.663	1.939

* 68 Degrees F -- 29.92 Inches of Mercury (Hg)

PROCESS DESCRIPTION AND OPERATION

3.1 General. Cumberland Paving Company, in Princeton, North Carolina, operates a continuous mix process to produce asphalt. An ASTEC rotary dryer, rated at 325 tons per hour, is used in the production process. The aggregate is dropped into the rotary dryer, where it is mixed, dried, and heated; liquid asphalt is then added to the aggregate and the product is transferred to a holding silo. The rotary dryer is fired with natural gas.

3.2 Process Emissions. Particulates are emitted from the process during drying and mixing due to the release of dust from the surface of the aggregate mix. The exhaust gases from the rotary dryer pass through a coater, baghouse, and a fan before exiting the stack to the atmosphere, as shown schematically in Figure 3-1.

3.3 Operation During Testing. Approximately 300 tons per hour of asphalt were produced during testing.

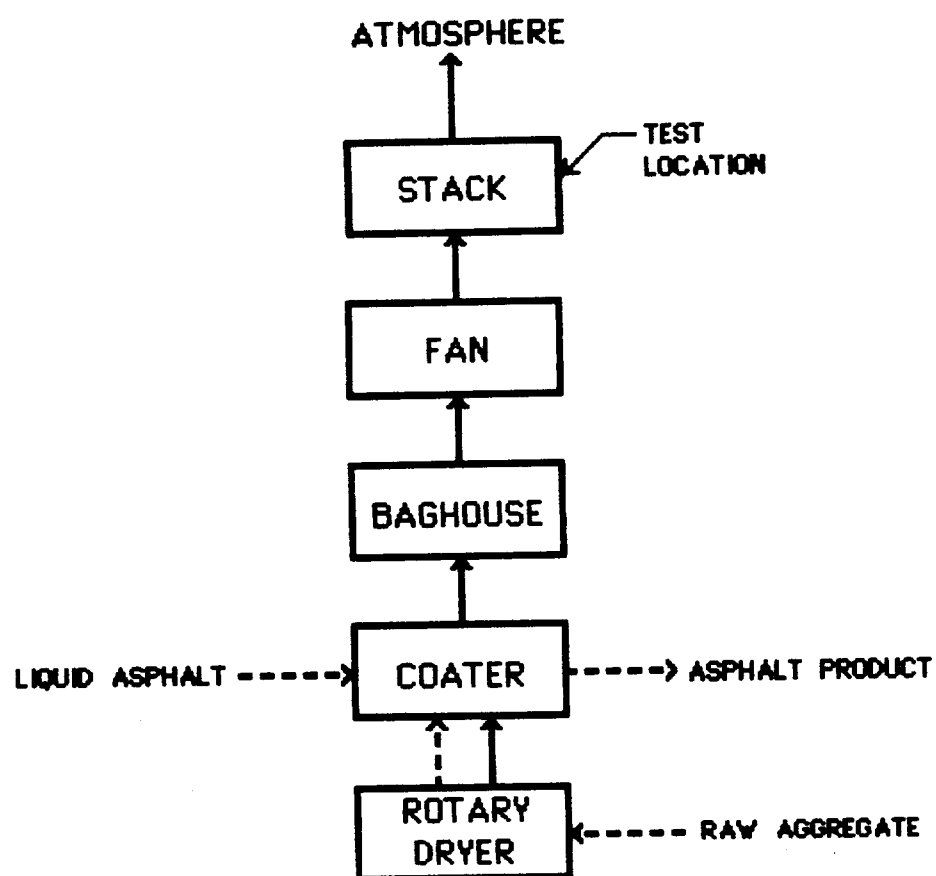


FIGURE 3-1. ROTARY DRYER AIR FLOW SCHEMATIC SHOWING TEST LOCATION

SAMPLING AND ANALYTICAL PROCEDURES

4.1 General. All sampling and analytical procedures were those recommended by the United States Environmental Protection Agency and the North Carolina Department of Natural Resources and Community Development. Descriptions of the sampling equipment and procedures (extracted from 40 CFR 60) are provided in Appendix D.

4.2 Sampling Points. The number and location of the sampling points were determined according to EPA Method 1. The stack cross section was divided into 24 equal areas, i.e., four sample points on each of the six traverse axes labeled A through F, as shown in Figure 4-1.

4.3 Volumetric Air Flow Rates

4.3.1 Flue Gas Velocity. EPA Method 2 was used to take the velocity measurements during the traverses of the stack cross section.

4.3.2 Flue Gas Composition. During run 2, a multipoint, integrated flue gas sample was collected and analyzed using EPA Method 3; the analytical results were used to determine the flue gas composition and molecular weight for each run.

4.3.3 Flue Gas Moisture. Moisture content was determined by analyzing the sampling train impinger reagents according to the procedures outlined in EPA Method 5.

4.4 Particulate Emissions. EPA Method 5 sampling and analytical procedures were used to determine the particulate emissions. The centroid of each of the 24 equal areas was sampled for 2.5 minutes, resulting in a net run time of 60 minutes.

4.5 Plume Opacity. The procedures outlined in EPA Method 9 were followed in determining the plume opacity.

4.6 Sampling Equipment. All sampling equipment was manufactured by Nutech Corporation or Entropy. Pertinent calibration data are provided in Appendix C.

TRAVERSE POINTS

6 AXES
4 POINTS/AXIS
24 TOTAL POINTS

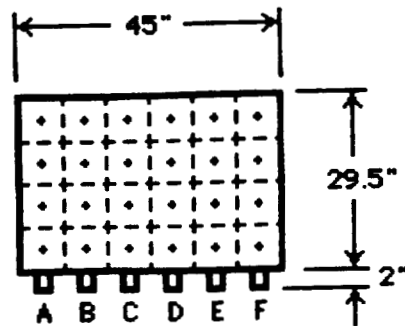
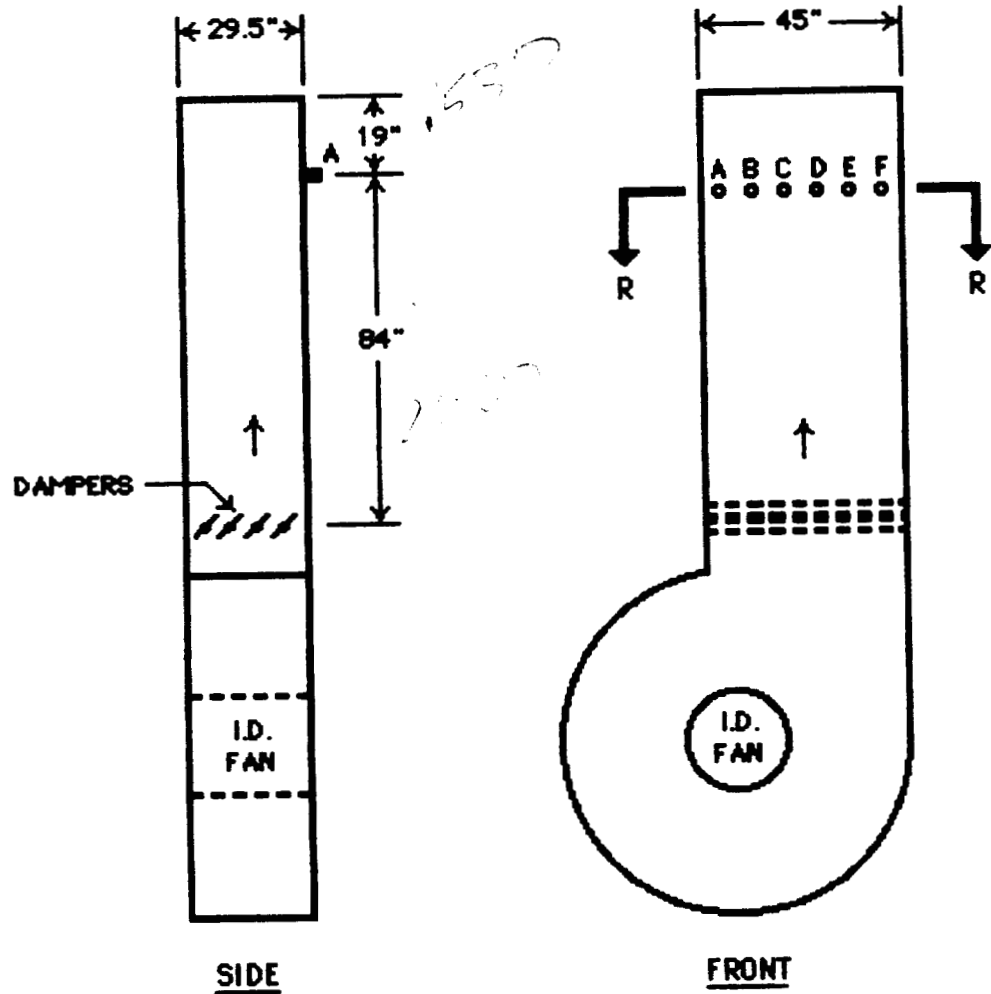
SECTION R-R

FIGURE 4-1. ROTARY DRYER BAGHOUSE STACK TEST LOCATION

APPENDIX A

TEST RESULTS AND EXAMPLE CALCULATIONS

ISOKINETIC SAMPLING TRAIN FIELD DATA & RESULTS TABULATION

PLANT: Cumberland Paving Princeton, NC

RUN #	DATE	SAMPLING LOCATION	OPERATOR		
1	6/29/87	Dryer Baghouse Stack	Arthur T. McDonald		
2	6/29/87	Dryer Baghouse Stack	Arthur T. McDonald		
3	6/29/87	Dryer Baghouse Stack	Arthur T. McDonald		
			1	2	3
			----	----	----
	Run Start Time		949	1308	1612
	Run Finish Time		1233	1528	1806
	Net Sampling Points		24	24	24
Theta	Net Run Time, Minutes		60.00	60.00	60.00
Dia	Nozzle Diameter, Inches		0.188	0.188	0.188
Cp	Pitot Tube Coefficient		0.840	0.840	0.840
Y	Dry Gas Meter Calibration Factor		0.997	0.997	0.997
Pbar	Barometric Pressure, Inches Hg		29.90	29.90	29.90
Delta H	Avg. Pressure Differential of Orifice Meter, Inches H2O		0.983	1.450	1.340
Vm	Volume of Metered Gas Sample, Dry ACP		32.757	39.604	38.934
tm	Dry Gas Meter Temperature, Degrees F		96	104	111
Vm(std)	Volume of Metered Gas Sample, Dry SCF*		31.056	37.057	35.974
Vlc	Total Volume of Liquid Collected in Impingers & Silica Gel, mL		101.5	125.0	111.0
Vw(std)	Volume of Water Vapor, SCF*		4.778	5.884	5.225
%H2O	Moisture Content, Percent by Volume		13.3	13.7	12.7
Mfd	Dry Mole Fraction		0.867	0.863	0.873
%CO2	Carbon Dioxide, Percent by Volume, Dry		4.0	4.0	4.0
%O2	Oxygen, Percent by Volume, Dry		15.0	15.0	15.0
%CO+N2	CO + N2, Percent by Volume, Dry		81.0	81.0	81.0
Md	Dry Molecular Weight, Lb/Lb-Mole		29.24	29.24	29.24
Ms	Wet Molecular Weight, Lb/Lb-Mole		27.74	27.70	27.81
Pg	Flue Gas Static Pressure, Inches H2O		-0.10	-1.05	-1.10
Ps	Absolute Flue Gas Press., Inches HG		29.89	29.82	29.82
ts	Flue Gas Temperature, Degrees F		275	270	259
Delta p	Average Velocity Head, Inches H2O		1.5730	1.5510	1.4880
vs	Flue Gas Velocity, Feet/Second		84.79	84.07	81.56
A	Stack/Duct Area, Square Inches		1,328	1,328	1,328
Qsd	Volumetric Air Flow Rate, Dry SCFM*		29,162	28,920	28,818
Qaw	Volumetric Air Flow Rate, Wet ACFM		46,900	46,502	45,113
%I	Isokinetic Sampling Rate, Percent		84.8	102.0	99.4
%EA	Excess Air, Percent		235.0	235.0	235.0

* 68 Degrees F -- 29.92 Inches of Mercury (Hg)

(continued next page)

		1	2	3
		----	----	----
	<u>Method 5 Results:</u>			
mg	Catch, Milligrams	27.7	25.8	18.3
gr/DSCF	Concentration, Grains per DSCF*	0.01376	0.01074	0.007850
Lb/Hr	Emission Rate, Lbs/Hour (PMRc)	3.441	2.663	1.939

* 68 Degrees F -- 29.92 Inches of Mercury (Hg)

EXAMPLE PARTICULATE TEST CALCULATIONS NO. 1

Dryer Baghouse Stack

VOLUME OF DRY GAS SAMPLED AT STANDARD CONDITIONS

$$V_m(\text{std}) = 17.64 * Y * V_m * \frac{(P_{\text{bar}} + \Delta H/13.6)}{(460 + t_m)}$$

$$V_m(\text{std}) = 17.64 * 0.997 * 32.757 * \frac{(29.90 + 0.983/13.6)}{(460 + 96)} = 31.056 \text{ DSCF}$$

VOLUME OF WATER VAPOR AT STANDARD CONDITIONS

$$V_w(\text{std}) = 0.04707 * V_{lc}$$

$$V_w(\text{std}) = 0.04707 * 101.5 = 4.778 \text{ SCF}$$

PERCENT MOISTURE, BY VOLUME, AS MEASURED IN FLUE GAS

$$\%H_2O = 100 * V_w(\text{std}) / (V_w(\text{std}) + V_m(\text{std}))$$

$$\%H_2O = \frac{4.778}{4.778 + 31.056} * 100 = 13.3 \%$$

DRY MOLE FRACTION OF FLUE GAS

$$M_{fd} = 1 - \%H_2O/100$$

$$M_{fd} = 1 - 13.3/100 = 0.867$$

DRY MOLECULAR WEIGHT OF FLUE GAS

$$M_d = \%CO_2 * 0.44 + \%O_2 * 0.32 + \%CO+N_2 * 0.28$$

$$M_d = 4.0 * 0.44 + 15.0 * 0.32 + 81.0 * 0.28 = 29.24 \text{ LB/LB-MOLE}$$

WET MOLECULAR WEIGHT OF FLUE GAS

$$M_s = (M_d * M_{fd}) + (0.18 * \%H_2O)$$

$$M_s = 29.24 * 0.867 + (0.18 * 13.3) = 27.74 \text{ LB/LB-MOLE}$$

ABSOLUTE FLUE GAS PRESSURE

$$P_s = P_{bar} + P_g / 13.6$$

$$P_s = 29.90 + (-0.0 / 13.6) = 29.89 \text{ IN. HG.}$$

AVERAGE FLUE GAS VELOCITY [Note: (Delta p)avg is square of avg sq. root]

$$v_s = 85.49 * C_p * \text{SQRT} \left[\frac{(\Delta p)_{avg} * (460 + t_s)}{P_s * M_s} \right]$$

$$v_s = 85.49 * 0.840 * \text{SQRT} \left[\frac{1.5730 * (460 + 275)}{29.89 * 27.74} \right] = 84.8 \text{ FT/SEC}$$

DRY VOLUMETRIC FLUE GAS FLOW RATE @ STANDARD CONDITIONS

$$Q_{sd} = \frac{60}{144} * M_{fd} * v_s * A * \frac{T_{std}}{t_s + 460} * \frac{P_s}{P_{std}}$$

$$Q_{sd} = \frac{60}{144} * 0.867 * 84.8 * 1,327.5 * \frac{528}{275 + 460} * \frac{29.89}{29.92}$$

$$Q_{sd} = 29,162 \text{ SCFM}$$

WET VOLUMETRIC STACK GAS FLOW RATE @ FLUE GAS CONDITIONS

$$Q_{aw} = 60 / 144 * v_s * A$$

$$Q_{aw} = 60 / 144 * 84.8 * 1,327.5 = 46,900 \text{ ACFM}$$

PERCENT ISOKINETIC OF SAMPLING RATE

$$\%I = \frac{P_{std}}{T_{std}} * \frac{100}{60} * \frac{(t_s + 460) * V_m(std)}{P_s * v_s * M_{fd} * \theta * \text{Area-nozzle, sq.ft.}}$$

$$\%I = \frac{29.92}{528} * \frac{100}{60} * \frac{(275 + 460) * 31.056}{29.89 * 84.8 * 0.867 * 60.00 * 0.0001928}$$

$$\%I = 84.8 \%$$

GRAINS PER DRY STANDARD CUBIC FOOT

$$\text{gr/DSCF} = \frac{7000}{453,592} * \frac{\text{mgs}}{V_m(\text{std})}$$

$$\text{gr/DSCF} = \frac{7000}{453,592} * \frac{27.7}{31.056} = 0.0138 \text{ gr/DSCF}$$

POUNDS PER HOUR

$$\text{Lb/Hr} = 60 / 7000 * \text{gr/DSCF} * Q_{sd}$$

$$\text{Lb/Hr} = 60/7000 * 0.0138 * 29,162 = 3.44 \text{ LB/HR}$$

PERCENT EXCESS AIR

$$\%EA = \frac{\%O_2 - (0.5 * \%CO)}{(0.264 * \%N_2) - (\%O_2 - (0.5 * \%CO))} * 100$$

$$\%EA = \frac{15.0 - (0.5 * 0.0)}{0.264 * 81.0 - (15.0 - (0.5 * 0.0))} * 100 = 235.0 \%$$

APPENDIX B

FIELD AND ANALYTICAL DATA

APPENDIX B

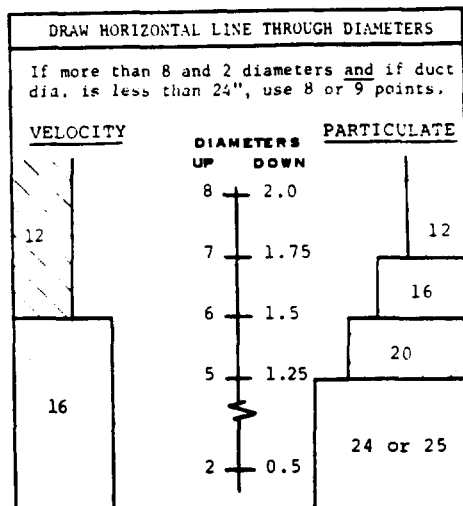
1. PARTICULATE

Preliminary Field Data

PLANT NAME Cumberland Paving Co.
 LOCATION Princeton NC.
 SAMPLING LOCATION Garhouse stack
 DUCT DEPTH
 FROM INSIDE FAR WALL TO OUTSIDE OF PORT 31 1/2"
 NIPPLE LENGTH 2"
 DEPTH OF DUCT 29 1/2"
 WIDTH (RECTANGULAR DUCT) 45"
 EQUIVALENT DIAMETER:

$$D_E = \frac{2 \times \text{DEPTH} \times \text{WIDTH}}{\text{DEPTH} + \text{WIDTH}} = \frac{2(29\frac{1}{2})(45)}{(29\frac{1}{2} + 45)} = 35\frac{5}{8}"$$

 DISTANCE FROM
 PORTS TO NEAREST UPSTREAM DOWNSTREAM
 FLOW DISTURBANCE 87" 19"
 DIAMETERS 2 1/2 1/2
 STACK AREA = 29 1/2" x 45" = 1327.5 IN²



Point	% OF DUCT DEPTH	DISTANCE FROM INSIDE WALL	DISTANCE FROM OUTSIDE OF PORT
1	12.5	3 5/8"	5 5/8"
2	37.5	11"	13"
3	62.5	18 3/8"	20 3/8"
4	87.5	25 7/8"	27 7/8"
5			
6			
7			
8			
9			
10			
11			
12			
13			
14			
15			
16			
17			
18			
19			
20			
21			
22			
23			
24			

LOCATION OF TRAVERSE POINTS IN CIRCULAR STACKS

	4	6	8	10	12	14	16	18	20	22	24
1	6.7	4.4	3.2	2.6	2.1	1.8	1.6	1.4	1.3	1.1	1.1
2	25.0	14.6	10.5	8.2	6.7	5.7	4.9	4.4	3.9	3.5	3.2
3	75.0	29.6	19.4	14.6	11.8	9.9	8.5	7.5	6.7	6.0	5.5
4	93.3	70.4	32.3	22.6	17.7	14.6	12.5	10.9	9.7	8.7	7.9
5		85.4	67.7	34.2	25.0	20.1	16.9	14.6	12.9	11.6	10.5
6		95.6	80.6	65.8	35.6	26.9	22.0	18.8	16.5	14.6	13.2
7			89.5	77.4	64.4	36.6	28.3	23.6	20.4	18.0	16.1
8			96.8	85.4	75.0	63.4	37.5	29.6	25.0	21.8	19.4
9				91.8	82.3	73.1	62.5	38.2	30.6	26.2	23.0
10				97.4	88.2	79.9	71.7	61.8	38.8	31.5	27.2
11					93.3	85.4	78.0	70.4	61.2	39.3	32.3
12					97.9	90.1	83.1	76.4	69.4	60.7	39.8
13						94.3	87.5	81.2	75.0	68.5	60.2
14						98.2	91.5	85.4	79.6	73.8	67.7
15							95.1	89.1	83.5	78.2	72.8
16							98.4	92.5	87.1	82.0	77.0
17								95.6	90.3	85.4	80.6
18								98.6	93.3	88.4	83.9
19									96.1	91.3	86.8
20									98.7	94.0	89.5
21										96.5	92.1
22										98.9	94.5
23											96.8
24											98.9

LOCATION OF TRAVERSE POINTS IN RECTANGULAR STACKS

	2	3	4	5	6	7	8	9	10	11	12
1	25.0	16.7	12.5	10.0	8.3	7.1	6.3	5.6	5.0	4.5	4.2
2	75.0	50.0	37.5	30.0	25.0	21.4	18.8	16.7	15.0	13.6	12.5
3		83.3	62.5	50.0	41.7	35.7	31.3	27.8	25.0	22.7	20.8
4			87.5	70.0	58.3	50.0	43.8	38.9	35.0	31.8	29.2
5				90.0	75.0	64.3	56.3	50.0	45.0	40.9	37.5
6					91.7	78.6	68.8	61.1	55.0	50.0	45.8
7						92.9	81.3	72.2	65.0	59.1	54.2
8							93.8	83.3	75.0	68.2	62.5
9								94.4	85.0	77.3	70.8
10									95.0	86.4	79.2
11										95.5	87.5
12											95.8

ORSAT FIELD DATA

Plant Name Chamberlain, Pringle - Princeton, NC
 Sampling Location Rotary Dryer, ^{baghouse} Stack Fuel Type #20.1

Run and/or Sample No. 2 Leak Test? ☒ Date 6/29/87 Operator WV

Time of Sample Collection	Time of Analysis	CO ₂ Reading A	O ₂ Reading B	CO Reading C	%O ₂ B-A	%CO C-B	%N ₂ 100-C
1308	1540	4.1	19.1	—	15.0		
to	to	4.0	19.0	—	15.0		
1528	1600	4.0	19.9	—	14.9		
Avg.		4.0		Avg.	15.0		81.0

Run and/or Sample No. _____ Leak Test? _____ Date _____ Operator _____

Time of Sample Collection	Time of Analysis	CO ₂ Reading A	O ₂ Reading B	CO Reading C	%O ₂ B-A	%CO C-B	%N ₂ 100-C
Avg.				Avg.			

Run and/or Sample No. _____ Leak Test? _____ Date _____ Operator _____

Time of Sample Collection	Time of Analysis	CO ₂ Reading A	O ₂ Reading B	CO Reading C	%O ₂ B-A	%CO C-B	%N ₂ 100-C
Avg.				Avg.			

PARTICULATE FIELD DATA

COMPANY NAME <u>Cumberland Paving Co.</u>		RUN NUMBER <u>1</u>	
ADDRESS <u>Smithfield NC Princeton, NC</u>		TIME START <u>0949</u>	
SAMPLING LOCATION <u>Baghouse Stack</u>		TIME FINISH <u>1233</u>	
DATE <u>6-29-87</u>		TECHNICIANS <u>MD</u>	
TEAM LEADER <u>THC</u>			
BAROMETRIC PRESSURE, IN. HG <u>29.9</u>		STATIC PRESSURE, IN. H ₂ O <u>-0.95</u>	
SAMPLING TRAIN LEAK TEST VACUUM, IN. HG <u>15</u>		<u>4</u>	
SAMPLING TRAIN LEAK RATE, CU. FT./MIN. <u>0.002</u>		<u>0.000</u>	

EQUIPMENT CHECKS	IDENTIFICATION NUMBERS
☒ PITOTS, PRE-TEST ☒ PITOTS, POST-TEST ☐ ORSAT SAMPLING SYSTEM ☐ TEDLAR BAG ☒ THERMOCOUPLE @ <u>300</u> °F	REAGENT BOX <u>0232</u> NOZZLE <u>501</u> DIAMETER <u>.188</u> METER BOX <u>114</u> T/C READOUT <u>Extack</u> UMBILICAL <u>12</u> T/C PROBE <u>4-3</u> SAMPLE BOX <u>3</u> ORSAT PUMP <u> </u> PROBE <u>4-3</u> TEDLAR BAG <u> </u>

FILTER #	TARE	NOMOGRAPH SET-UP	NOMOGRAPH # <u>1A2</u>
<u>E5228</u>	<u>.5146</u>	ΔH_0 <u>1.75</u> METER TEMP <u>80</u> / <u>100</u> % MOISTURE <u>30</u>	C FACTOR <u>0.67</u> / <u>0.61</u> STACK TEMP <u>300</u> REF. ΔP <u>3.40</u> / <u>3.20</u>

SAMPLE POINT	CLOCK TIME, MIN.	DRY GAS METER READING, CU. FT.	PITOT READING (ΔP), IN. H ₂ O	ORIFICE SETTING (ΔH), IN. H ₂ O		GAS METER TEMP. °F	PUMP VACUUM IN. HG GAUGE	FILTER BOX TEMP. °F	IMP. EXIT TEMP. °F	STACK TEMP. °F	LK. CHECK READINGS
				IDEAL	ACTUAL						
A 1	0/0	943.707	3.60	2.07	2.07	86	4	245	62	282	
2	2 1/2	946.017	3.55	2.04	2.04	88	4	248	60	284	
3	5	947.80	3.20	1.84	1.84	89	4	250	60	287	
4	7 1/2	949.58	1.50	0.86	0.86	90	4	250	61	288	
B 1	10/0	950.96	2.65	1.52	1.52	91	3	251	61	281	
2	2 1/2	952.72	2.55	1.47	1.47	92	3	251	62	283	
3	5	954.42	2.60	1.50	1.50	93	3	250	63	286	
4	7 1/2	956.18	2.00	1.15	1.15	94	3	250	63	287	
C 1	20/0	957.706	2.40	1.38	1.38	95	3	250	62	291	
2	2 1/2	959.39	1.75	1.01	1.01	95	3	251	62	291	
3	5	960.85	1.50	0.86	0.86	96	2	250	63	289	
4	7 1/2	962.22	2.00	1.15	1.15	96	3	252	64	274	
D 1	30/0	963.76	2.50	1.44	1.44	97	3	252	63	279	
2	2 1/2	965.45	1.05	0.60	0.60	97	3	255	63	285	
3	5	966.67	1.00	0.58	0.58	96	3	254	64	286	Fyrite 4%
4	7 1/2	968.80	0.83	0.48	0.48	97	3	252	63	281	
E 1	40/0	968.74	0.120	0.69	0.69	97	3	250	64	260	
2	2 1/2	969.95	0.75	0.43	0.43	99	2	248	65	261	
3	5	970.92	0.90	0.52	0.52	101	2	248	68	233	
4	7 1/2	972.02	0.95	0.55	0.55	100	2	251	67	258	
F 1	50/0	972.99	0.83	0.48	0.48	100	2	252	67	263	
2	2 1/2	974.05	0.39	0.22	0.22	101	2	253	66	260	
3	5	974.72	0.60	0.35	0.35	101	2	253	66	253	Fyrite 3%
4	7 1/2	975.58	0.69	0.40	0.40	101	2	253	65	248	
	60/0	976.464									

32.757 1.573

.9929 96

279

PARTICULATE FIELD DATA

COMPANY NAME <u>Cumberland Mining Co</u>		RUN NUMBER <u>2</u>	
ADDRESS <u>Smithfield NC</u>		TIME START <u>1302</u>	
SAMPLING LOCATION <u>Baghouse stack</u>		TIME FINISH <u>1528</u>	
DATE <u>6-29-82</u>		TECHNICIANS <u>MO</u>	
TEAM LEADER <u>Thy</u>			
BAROMETRIC PRESSURE, IN. HG <u>29.9</u>		STATIC PRESSURE, IN. H ₂ O <u>-1.05</u>	
SAMPLING TRAIN LEAK TEST VACUUM, IN. HG <u>15</u>		<u>6</u>	
SAMPLING TRAIN LEAK RATE, CU. FT./MIN. <u>0.001</u>		<u>0.000</u>	

EQUIPMENT CHECKS ☒ PITOTS, PRE-TEST ☒ PITOTS, POST-TEST ☒ ORSAT SAMPLING SYSTEM ☒ TEDLAR BAG ☒ THERMOCOUPLE @ <u>280</u> °F	IDENTIFICATION NUMBERS REAGENT BOX <u>0232</u> NOZZLE <u>501</u> DIAMETER <u>.188</u> METER BOX <u>N4</u> T/C READOUT <u>attach</u> UMBILICAL <u>12</u> T/C PROBE <u>6-3</u> SAMPLE BOX <u>5</u> ORSAT PUMP <u>581</u> PROBE <u>4-5</u> TEDLAR BAG <u>6</u>
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FILTER # <u>85729</u>	TARE <u>.5082</u>	NOMOGRAPH SET-UP ΔH ₀ <u>1.75</u> METER TEMP <u>105</u> % MOISTURE <u>14</u>	NOMOGRAPH # <u>(VAD)</u> C FACTOR <u>0.86</u> STACK TEMP <u>280</u> REF. ΔP <u>2.18</u>
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SAMPLE POINT	CLOCK TIME, MIN.	DRY GAS METER READING, CU. FT.	PITOT READING (ΔP), IN. H ₂ O	ORIFICE SETTING (ΔH), IN. H ₂ O		GAS METER TEMP. °F	PUMP VACUUM IN. HG GAUGE	FILTER BOX TEMP. °F	IMP. EXIT TEMP. °F	STACK TEMP. °F	LK. CHECK READINGS
				IDEAL	ACTUAL						
A1	0/0	976.591	3.80	3.28	3.21	100	6	255	61	276	
2	2 1/2	979.20	4.00	3.34	3.34	101	6	255	63	278	
3	5	981.68	2.90	2.45	2.45	102	5	254	63	279	Fails 470
4	7 1/2	983.96	1.55	1.31	1.31	102	3	254	61	280	
B1	10/0	985.69	2.10	1.77	1.77	102	4	255	61	283	
2	2 1/2	987.60	2.80	2.36	2.36	102	5	254	63	278	
3	5	989.74	2.60	2.19	2.19	102	5	254	63	276	
4	7 1/2	991.80	1.85	1.56	1.56	104	4	252	64	275	
C1	20/0	993.61	2.45	2.07	2.07	105	5	252	65	271	
2	2 1/2	995.83	1.95	1.65	1.65	105	4	250	65	268	
3	5	997.61	1.98	1.67	1.67	102	4	253	68	252	
4	7 1/2	999.46	1.75	1.48	1.48	102	4	255	64	234	
D1	30/0	1001.15	1.45	1.22	1.22	103	3	256	62	270	
2	2 1/2	2.76	1.05	0.89	0.89	103	2	254	62	266	
3	5	4.18	1.20	1.01	1.01	103	2	254	63	269	
4	7 1/2	5.60	1.00	0.84	0.84	103	2	255	61	271	
E1	40/0	6.95	1.60	1.35	1.35	103	3	257	63	272	
2	2 1/2	8.63	0.55	0.46	0.46	104	2	257	64	272	
3	5	9.69	1.08	0.91	0.91	104	2	256	64	274	
4	7 1/2	11.06	0.65	0.55	0.55	105	2	256	66	275	
F1	50/0	12.15	0.74	0.62	0.62	105	2	257	66	273	
2	2 1/2	13.28	0.33	0.28	0.28	109	1	259	67	258	
3	5	14.08	0.66	0.56	0.56	109	2	258	65	261	
4	7 1/2	15.16	0.61	0.51	0.51	109	2	256	67	262	
	40/0	1016.195									

39.604
1.551
1.446 104
270

PARTICULATE FIELD DATA

COMPANY NAME <u>Cumberland Mining Co</u>		RUN NUMBER <u>3</u>	
ADDRESS <u>Princeton NC</u>		TIME START <u>1612</u>	
SAMPLING LOCATION <u>Baghouse Street</u>		TIME FINISH <u>1806</u>	
DATE <u>6-29-82</u>		TEAM LEADER <u>THD</u> TECHNICIANS <u>MO</u>	
BAROMETRIC PRESSURE, IN. HG <u>29.9</u>		STATIC PRESSURE, IN. H ₂ O <u>-1.10</u>	
SAMPLING TRAIN LEAK TEST VACUUM, IN. HG <u>15</u> <u>6</u>			
SAMPLING TRAIN LEAK RATE, CU. FT./MIN. <u>0.001</u> <u>0.001</u>			

EQUIPMENT CHECKS ☒ PITOTS, PRE-TEST ☐ PITOTS, POST-TEST ☐ ORSAT SAMPLING SYSTEM ☐ TEDLAR BAG ☒ THERMOCOUPLE @ <u>280</u> °F	IDENTIFICATION NUMBERS REAGENT BOX <u>0332</u> NOZZLE <u>501</u> DIAMETER <u>.188</u> METER BOX <u>U4</u> T/C READOUT <u>Extach</u> UMBILICAL <u>U2</u> T/C PROBE <u>6-3</u> SAMPLE BOX <u>3</u> ORSAT PUMP _____ PROBE <u>4-3</u> TEDLAR BAG _____
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FILTER # <u>25730</u> TARE <u>.5015</u> _____ _____	NOMOGRAPH SET-UP NOMOGRAPH # <u>YAD</u> ΔH _g <u>1.75</u> C FACTOR <u>0.66</u> METER TEMP <u>105</u> STACK TEMP <u>180</u> % MOISTURE <u>14</u> REF. ΔP <u>2.18</u>
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SAMPLE POINT	CLOCK TIME, MIN.	DRY GAS METER READING, CU. FT.	PITOT READING (ΔP), IN. H ₂ O	ORIFICE SETTING (ΔH), IN. H ₂ O		GAS METER TEMP. °F	PUMP VACUUM IN. HG GAUGE	FILTER BOX TEMP. °F	IMP. EXIT TEMP. °F	STACK TEMP. °F	LK. CHECK READINGS
				IDEAL	ACTUAL						
A1	0/0	16.300	3.10	2.62	2.62	106	6	263	68	258	
2	2 1/2	18.67	2.95	2.49	2.49	107	6	262	64	255	
3	5	20.91	1.90	1.60	1.60	108	5	260	63	261	
4	7 1/2	22.81	1.85	1.31	1.31	109	4	260	63	249	
B1	10/0	24.45	2.10	1.77	1.77	109	5	257	64	249	
2	2 1/2	26.37	1.85	1.56	1.56	110	5	258	64	254	
3	5	28.18	2.65	2.24	2.24	110	6	257	65	255	
4	7 1/2	30.29	1.85	1.56	1.56	112	5	257	65	256	
C1	20/0	32.12	2.90	2.45	2.45	111	4	255	67	260	
2	2 1/2	34.24	1.30	1.10	1.10	112	3	253	69	247	
3	5	35.79	1.68	1.42	1.42	111	3	253	68	249	
4	7 1/2	37.53	1.89	1.60	1.60	111	3	254	68	247	
D1	30/0	39.35	1.47	1.24	1.24	112	3	255	67	258	
2	2 1/2	40.97	1.00	0.84	0.84	112	2	254	63	258	
3	5	42.41	1.38	1.16	1.16	112	2	254	63	260	
4	7 1/2	43.93	1.85	1.56	1.56	112	3	253	64	262	
E1	40/0	45.72	0.97	0.82	0.82	112	2	254	64	261	
2	2 1/2	47.06	0.56	0.47	0.47	112	2	253	66	263	
3	5	48.06	0.99	0.84	0.84	112	2	253	66	268	
4	7 1/2	49.38	0.38	1.16	1.16	111	2	254	67	270	freite 4%
F1	50/0	50.95	1.07	0.90	0.90	111	2	254	67	272	
2	2 1/2	52.34	0.34	0.29	0.29	111	2	253	68	269	
3	5	53.14	0.48	0.41	0.41	111	2	253	68	268	
4	7 1/2	54.08	0.82	0.69	0.69	111	2	255	69	271	
	60/0	55.234									

38.934 1.488

1.338 111

259

PARTICULATE SAMPLING LABORATORY RESULTS

Plant Name CUMBERLAND PAVING EEI Ref. # 5569

Sampling Location BACHOUSE STACK

Date Received 6/30 Date Analyzed 7/2 Reagent Box(es) 0232

Run Number	<u>1</u>	<u>2</u>	<u>3</u>
Run Date	<u>6/29</u>	<u>6/29</u>	<u>6/29</u>

SUMMARY OF PARTICULATE ANALYSES

Sum of Particulate, mg.	<u>542.6</u>	<u>534.2</u>	<u>519.9</u>
Total Filter Tare mg.	<u>514.6</u>	<u>508.2</u>	<u>501.5</u>
Blank Residue, mg. (<u>125</u> mL)	<u>0.3</u>	(<u>100</u> mL) <u>0.2</u>	(<u>50</u> mL) <u>0.1</u>
TOTAL PARTICULATE CATCH, mg.	<u>27.7</u>	<u>25.8</u>	<u>18.3</u>

ANALYSIS OF MOISTURE CATCH

<u>Reagent 1 (H₂O):</u>			
Final Weight, g.	<u>280.0</u>	<u>310.0</u>	<u>290.0</u>
Tared Weight, g.	<u>200.0</u>	<u>200.0</u>	<u>200.0</u>
Water Catch, g.	<u>80.0</u>	<u>110.0</u>	<u>90.0</u>
<u>Reagent 2 ()::</u>			
Final Weight, g.	<u>-</u>	<u>-</u>	<u>-</u>
Tared Weight, g.	<u>-</u>	<u>-</u>	<u>-</u>
Water Catch, g.	<u>-</u>	<u>-</u>	<u>-</u>
CONDENSED WATER, g.	<u>80.0</u>	<u>110.0</u>	<u>90.0</u>
<u>Silica Gel:</u>			
Final Weight, g.	<u>221.5</u>	<u>215.0</u>	<u>221.0</u>
Tared Weight, g.	<u>200.0</u>	<u>200.0</u>	<u>200.0</u>
ADSORBED WATER, g.	<u>21.5</u>	<u>15.0</u>	<u>21.0</u>
TOTAL WATER COLLECTED, g.	<u>101.5</u>	<u>125.0</u>	<u>111.0</u>

Blank Beaker # 2015

Final wt. mg. 94782.1

Tare wt. mg. 94781.7

Residue, mg. 0.4

Volume, mL. 200.0

Concen., mg/mL .002

--- Legend ---

= Final Weight

L = Loose Particulate

F = Filter D = Dish

R = Rinse P = Pan

Notes and Comments

ENTROPY

LABORATORY SAMPLE WEIGHT CALCULATIONS

Plant Name CUMBERLAND PAVING

EEI Ref. # 5569

Run Number

1

2

3

Run Date

6/29

6/29

6/29

Sample ID/Container #

FLR 384

FLR 398

FLR 463

Tare Wt., g.

133.8589
✓ 133.8586
133.8600
133.3160

✓ 124.5930
124.5930
124.0588

✓ 134.7335
134.7335
134.2136

SAMPLE WT., g.

.5426

.5342

.5199

Sample ID/Container #

Tare Wt., g.

SAMPLE WT., g.

Sample ID/Container #

Tare Wt., g.

SAMPLE WT., g.

Sample ID/Container #

Tare Wt., g.

SAMPLE WT., g.

ENTROPY

CUSTODY SHEET FOR REAGENT BOX # 0232

Date of Makeup 6/26 Initials MS Locked? ☒
 Individual Tare of Reagent: 200 mls. of H₂O
 Individual Tare of Reagent: _____ mls. of _____
 Individual Silica Gel Tare Weight 200 gms.

PLANT NAME Cumberland Paving Co.SAMPLING LOCATION Baghouse Stack

Run Number	Date Used	Initials	Locked?	Date Cleanup	% S. Gel Spent	Initials	Locked?
1	6-29-87	<u>MS</u>	☒	6-29-87	40	<u>MS</u>	☒
2	6-29-87	<u>↓</u>	☒	6-29-87	40	<u>↓</u>	☒
3	6-29-87	<u>↓</u>	☒	6-29-87	40	<u>↓</u>	☒

Received in Lab 6/30 Date J.F.J. Initials ✓ Locked?

Sampling Method: MSZero & Span Balance Initials J.F.J.

Filter # Tare Weight (grams) Used on Test

Remarks:

<u>ES725</u>	<u>.5786</u>	<u>1</u>
<u>ES729</u>	<u>.5082</u>	<u>2</u>
<u>ES730</u>	<u>.5015</u>	<u>3</u>
_____	_____	_____
_____	_____	_____
_____	_____	_____

APPENDIX B

2. PLUME OPACITY

VISIBLE EMISSION OBSERVATION FORM

No. 1-1

COMPANY NAME <u>Cumberland Paving Co.</u>		
STREET ADDRESS		
CITY <u>Princeton</u>	STATE <u>NC</u>	ZIP
PHONE (KEY CONTACT)	SOURCE ID NUMBER	

PROCESS EQUIPMENT <u>Asphalt Plant</u>	OPERATING MODE
CONTROL EQUIPMENT <u>Baghouse</u>	OPERATING MODE

DESCRIBE EMISSION POINT <u>Rectangle Stack</u> <u>Baghouse Stack</u>	
HEIGHT ABOVE GROUND LEVEL <u>20'</u>	HEIGHT RELATIVE TO OBSERVER Start <u>20'</u> End <u>20'</u>
DISTANCE FROM OBSERVER Start <u>40'</u> End <u>30'</u>	DIRECTION FROM OBSERVER Start <u>SW</u> End <u>SW</u>

DESCRIBE EMISSIONS Start <u>0</u> End <u>0</u>	
EMISSION COLOR Start <u>0</u> End <u>0</u>	IF WATER DROPLET PLUME Attached ☐ Detached ☐
POINT IN THE PLUME AT WHICH OPACITY WAS DETERMINED Start <u>Stack Exit</u> End <u>Same</u>	

DESCRIBE PLUME BACKGROUND Start <u>Blue Sky</u> End <u>Same</u>	
BACKGROUND COLOR Start <u>Blue</u> End <u></u>	SKY CONDITIONS Start <u>Clear</u> End <u></u>
WIND SPEED Start <u>0-5 mph</u> End <u></u>	WIND DIRECTION Start <u>SW</u> End <u></u>
AMBIENT TEMP Start <u>85</u> End <u></u>	WET BULB TEMP RH, percent

Stack with Plume Sun Wind	SOURCE LAYOUT SKETCH
---------------------------------	--------------------------

ADDITIONAL INFORMATION

OBSERVATION DATE		START TIME		END TIME	
4/29/87		9:49		1135	
SEC	0	15	30	45	COMMENTS
MIN					
1	0	0	0	0	
2	0	0	0	0	
3	0	0	0	0	
4	0	0	0	0	
5	0	0	0	0	
6	0	0	0	0	
7	0	0	0	0	
8	0	0	0	0	
9	0	0	0	0	
10	0	0	0	0	
11	0	0	0	0	
12	0	0	0	0	
13	0	0	0	0	
14	0	0	0	0	
15	0	0	0	0	
16	0	0	0	0	
17	0	0	0	0	
18	0	0	0	0	
19	0	0	0	0	
20	0	0	0	0	
21	0	0	0	0	
22	0	0	0	0	
23	0	0	0	0	
24	0	0	0	0	
25	0	0	0	0	
26	0	0	0	0	
27	0	0	0	0	
28	0	0	0	0	
29	0	0	0	0	
30	0	0	0	0	

OBSERVER'S NAME (PRINT) <u>Michael Kirkman</u>	DATE <u>6/29/87</u>
OBSERVER'S SIGNATURE <u>Michael Kirkman</u>	
ORGANIZATION <u>Entropy</u>	
CERTIFIED BY <u>Eastern Tech. Assoc</u>	DATE <u>5/13/87</u>
CONTINUED ON VEO FORM NUMBER	<u>1-2</u>

VISIBLE EMISSION OBSERVATION FORM

No. 1-2

COMPANY NAME <i>Cumberland Paving Co.</i>		
STREET ADDRESS		
CITY <i>Princeton</i>	STATE <i>NC</i>	ZIP
PHONE (KEY CONTACT)	SOURCE ID NUMBER	

PROCESS EQUIPMENT	OPERATING MODE
CONTROL EQUIPMENT	OPERATING MODE

DESCRIBE EMISSION POINT <i>Baghouse Stack</i>	
HEIGHT ABOVE GROUND LEVEL	HEIGHT RELATIVE TO OBSERVER Start End
DISTANCE FROM OBSERVER Start End	DIRECTION FROM OBSERVER Start End

DESCRIBE EMISSIONS	
Start End	
EMISSION COLOR	IF WATER DROPLET PLUME Attached ☐ Detached ☐
Start End	
POINT IN THE PLUME AT WHICH OPACITY WAS DETERMINED Start End	

DESCRIBE PLUME BACKGROUND	
Start End	
BACKGROUND COLOR	SKY CONDITIONS
Start End	Start End
WIND SPEED	WIND DIRECTION
Start End	Start End
AMBIENT TEMP	WET BULB TEMP RH, percent
Start End	

Stack with Plume Sun Wind	SOURCE LAYOUT SKETCH Draw North Arrow
---------------------------------	--

ADDITIONAL INFORMATION

OBSERVATION DATE				START TIME	END TIME
6/29/87					
SEC	0	15	30	45	COMMENTS
MIN					
1	0	0	0	0	
2	0	0	0	0	
3	0	0	0	0	
4	0	0	0	0	
5	0	0	0	0	
6	0	0	0	0	stopped 1025 started 1059
7	0	0	0	0	
8	0	0	0	0	
9	0	0	0	0	
10	0	0	0	0	
11	0	0	0	0	
12	0	0	0	0	
13	0	0	0	0	
14	0	0	0	0	
15	0	0	0	0	
16	0	0	0	0	
17	0	0	0	0	
18	0	0	0	0	
19	0	0	0	0	
20	0	0	0	0	
21	0	0	0	0	
22	0	0	0	0	
23	0	0	0	0	
24	0	0	0	0	stopped 1118 started 1130
25	0	0	0	0	
26	0	0	0	0	
27	0	0	0	0	
28	0	0	0	0	
29	0	0	0	0	
30	0	0	0	0	

OBSERVER'S NAME (PRINT)	
OBSERVER'S SIGNATURE <i>Michael L. ...</i>	DATE <i>6/29/87</i>
ORGANIZATION	
CERTIFIED BY	DATE
CONTINUED ON VEO FORM NUMBER	

E N D

VISIBLE EMISSION OBSERVATION FORM

No.

2-1

COMPANY NAME
Cumberland Paving Co.

STREET ADDRESS

CITY
Princeton

STATE
NC

ZIP

PHONE (KEY CONTACT)

SOURCE ID NUMBER

PROCESS EQUIPMENT
Asphalt Plant

OPERATING MODE

CONTROL EQUIPMENT
Baghouse

OPERATING MODE

DESCRIBE EMISSION POINT
Rectangular Stack
Baghouse Stack

HEIGHT ABOVE GROUND LEVEL
20'

HEIGHT RELATIVE TO OBSERVER
Start *17'* End

DISTANCE FROM OBSERVER
Start *35'* End

DIRECTION FROM OBSERVER
Start *NW* End

DESCRIBE EMISSIONS

Start *0* End *0*

EMISSION COLOR
Start *0* End *0*

IF WATER DROPLET PLUME
Attached ☐ Detached ☐

POINT IN THE PLUME AT WHICH OPACITY WAS DETERMINED
Stack Exit End *Same*

DESCRIBE PLUME BACKGROUND

Start *SKY* End *SKY*

BACKGROUND COLOR
Start *Blue* End *Blue*

SKY CONDITIONS
Start *Clear* End *Clear*

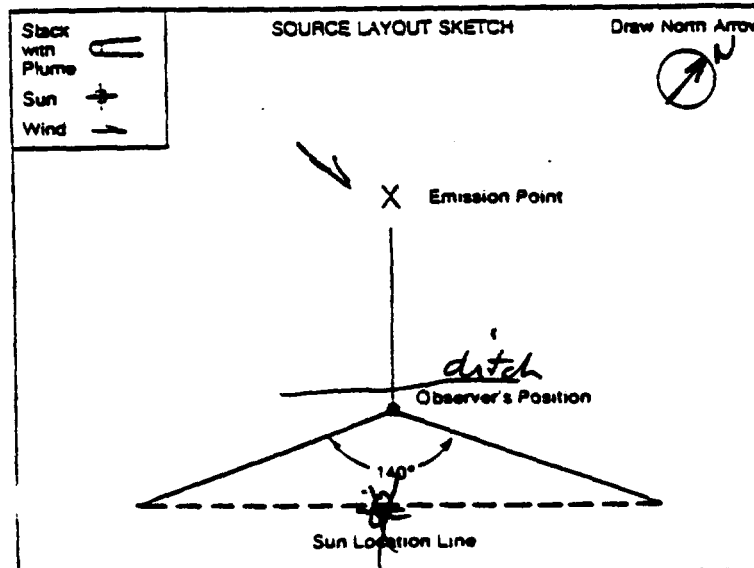
WIND SPEED
Start *0-5 mph* End *0-5*

WIND DIRECTION
Start *W* End *W*

AMBIENT TEMP
Start *88* End *88*

WET BULB TEMP

RM, percent



ADDITIONAL INFORMATION

OBSERVATION DATE		START TIME				END TIME
6/29/87		1313				1506
SEC	0	15	30	45	COMMENTS	
MIN						
1	0	0	0	0		
2	0	0	0	0		
3	0	0	0	0		
4	0	0	0	0		
5	0	0	0	0		
6	0	0	0	0		
7	0	0	0	0		
8	0	0	0	0		
9	0	0	0	0		
10	0	0	0	0		
11	0	0	0	0		
12	0	0	0	0		
13	0	0	0	0		
14	0	0	0	0		
15	0	0	0	0		
16	0	0	0	0		
17	0	0	0	0		
18	0	0	0	0		
19	0	0	0	0		
20	0	0	0	0		
21	0	0	0	0		
22	0	0	0	0		
23	0	0	0	0		
24	0	0	0	0		
25	0	0	0	0	stopped 1340	
26	0	0	0	0		
27	0	0	0	0	stopped 1450	
28	0	0	0	0		
29	0	0	0	0		
30	0	0	0	0		

OBSERVER'S NAME (PRINT)
Michael Kirkman

OBSERVER'S SIGNATURE
Michael Kirkman

DATE
6/29/87

ORGANIZATION
Entropy

CERTIFIED BY
Eastern Tech Assoc.

DATE
5/13/87

CONTINUED ON VEO FORM NUMBER
2-2

VISIBLE EMISSION OBSERVATION FORM

No. 2-2

COMPANY NAME
Cumberland Packing Co.
STREET ADDRESS

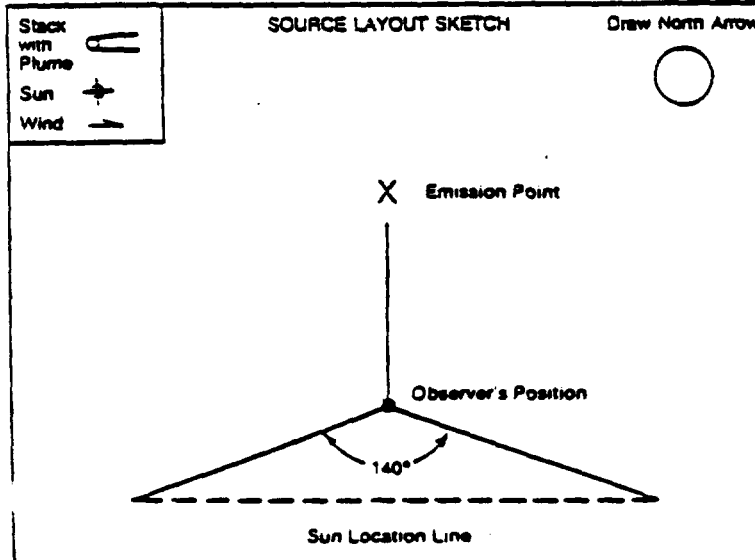
CITY *Princeton* STATE *NC* ZIP
PHONE (KEY CONTACT) SOURCE ID NUMBER

PROCESS EQUIPMENT OPERATING MODE
CONTROL EQUIPMENT OPERATING MODE

DESCRIBE EMISSION POINT
Stack
HEIGHT ABOVE GROUND LEVEL HEIGHT RELATIVE TO OBSERVER
Start End
DISTANCE FROM OBSERVER DIRECTION FROM OBSERVER
Start End Start End

DESCRIBE EMISSIONS
Start End
EMISSION COLOR IF WATER DROPLET PLUME
Start End Attached ☐ Detached ☐
POINT IN THE PLUME AT WHICH OPACITY WAS DETERMINED
End

DESCRIBE PLUME BACKGROUND
Start End
BACKGROUND COLOR SKY CONDITIONS
Start End Start End
WIND SPEED WIND DIRECTION
Start End Start End
AMBIENT TEMP WET BULB TEMP RH, percent
Start End



ADDITIONAL INFORMATION

OBSERVATION DATE		START TIME				END TIME
<i>6/29/87</i>						
SEC	MIN	0	15	30	45	COMMENTS
1	0	0	0	0		
2	0	0	0	0		
3	0	0	0	0		
4	0	0	0	0		
5	0	0	0	0		
6	0	0	0	0		
7	0	0	0	0		
8	0	0	0	0		
9	0	0	0	0		
10	0	0	0	0		
11	0	0	0	0		
12	0	0	0	0		
13	0	0	0	0		
14	0	0	0	0		
15	0	0	0	0		
16	0	0	0	0		
17	0	0	0	0		
18	0	0	0	0		<i>stopped 1455</i>
19	0	0	0	0		<i>started 1456</i>
20	0	0	0	0		
21	0	0	0	0		
22	0	0	0	0		
23	0	0	0	0		
24	0	0	0	0		
25	0	0	0	0		
26	0	0	0	0		
27	0	0	0	0		
28	0	0	0	0		
29	0	0	0	0		
30	0	0	0	0		

OBSERVER'S NAME (PRINT)
OBSERVER'S SIGNATURE *Michael R. Kahan* DATE *6/29/87*
ORGANIZATION
CERTIFIED BY DATE
CONTINUED ON VEO FORM NUMBER *END*

VISIBLE EMISSION OBSERVATION FORM

No. 3-1

COMPANY NAME
Cumberland Paving Co

STREET ADDRESS

CITY *Princeton* STATE *NC* ZIP

PHONE (KEY CONTACT) SOURCE ID NUMBER

PROCESS EQUIPMENT *Asphalt Plant* OPERATING MODE

CONTROL EQUIPMENT *Baghouse* OPERATING MODE

DESCRIBE EMISSION POINT
Rectangular Stack
Baghouse Stack

HEIGHT ABOVE GROUND LEVEL *20'* HEIGHT RELATIVE TO OBSERVER
Start *20'* End *20'*

DISTANCE FROM OBSERVER *70'* DIRECTION FROM OBSERVER
Start *SE* End *SE*

DESCRIBE EMISSIONS
Start *0* End *0*

EMISSION COLOR *0* IF WATER DROPLET PLUME
Start *0* End *0* Attached ☐ Detached ☐

POINT IN THE PLUME AT WHICH OPACITY WAS DETERMINED
Stack Exit End *Same*

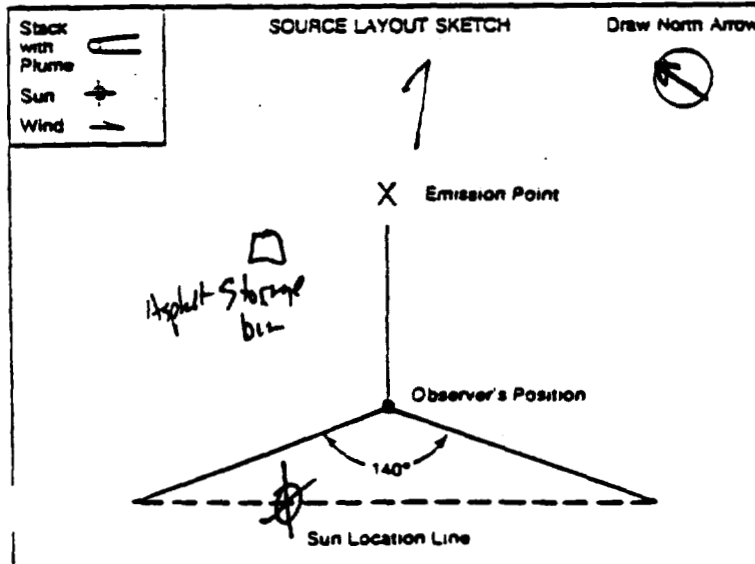
DESCRIBE PLUME BACKGROUND
Start *SKY* End *SKY*

BACKGROUND COLOR *Blue* SKY CONDITIONS *Clear* End *Partly Cloudy*

WIND SPEED *5 mph* WIND DIRECTION *SW* End

AMBIENT TEMP *88* WET BULB TEMP RH, percent

Start *88* End *82*



ADDITIONAL INFORMATION

OBSERVATION DATE		START TIME				END TIME
6/29/87		1615				1755
SEC	0	15	30	45	COMMENTS	
MIN						
1	0	0	0	0		
2	0	0	0	0		
3	0	0	0	0		
4	0	0	0	0		
5	0	0	0	0		
6	0	0	0	0		
7	0	0	0	0		
8	0	0	0	0		
9	0	0	0	0		
10	0	0	0	0		
11	0	0	0	0		
12	0	0	0	0		
13	0	0	0	0		
14	0	0	0	0		
15	0	0	0	0		
16	0	0	0	0		
17	0	0	0	0		
18	0	0	0	0		
19	0	0	0	0		
20	0	0	0	0		
21	0	0	0	0		
22	0	0	0	0		
23	0	0	0	0		
24	0	0	0	0		
25	0	0	0	0		
26	0	0	0	0		
27	0	0	0	0		
28	0	0	0	0		
29	0	0	0	0		
30	0	0	0	0	stopped 1645	

OBSERVER'S NAME (PRINT) *Michael Kinkaman*

OBSERVER'S SIGNATURE *Michael Kinkaman* DATE *6/29/87*

ORGANIZATION *Entropy*

CERTIFIED BY *Eastern Tech Assoc.* DATE *5/13/87*

CONTINUED ON VEO FORM NUMBER *3-2*

VISIBLE EMISSION OBSERVATION FORM

No.

3-2

COMPANY NAME
Cummins Inc.

STREET ADDRESS

CITY
Hamlet

STATE
NC

ZIP

PHONE (KEY CONTACT)

SOURCE ID NUMBER

PROCESS EQUIPMENT

OPERATING MODE

CONTROL EQUIPMENT

OPERATING MODE

DESCRIBE EMISSION POINT
Bay House Stack

HEIGHT ABOVE GROUND LEVEL

HEIGHT RELATIVE TO OBSERVER
Start End

DISTANCE FROM OBSERVER

DIRECTION FROM OBSERVER
Start End

DESCRIBE EMISSIONS

Start End

EMISSION COLOR

IF WATER DROPLET PLUME
Attached ☐ Detached ☐

POINT IN THE PLUME AT WHICH OPACITY WAS DETERMINED
Start End

DESCRIBE PLUME BACKGROUND

Start End

BACKGROUND COLOR

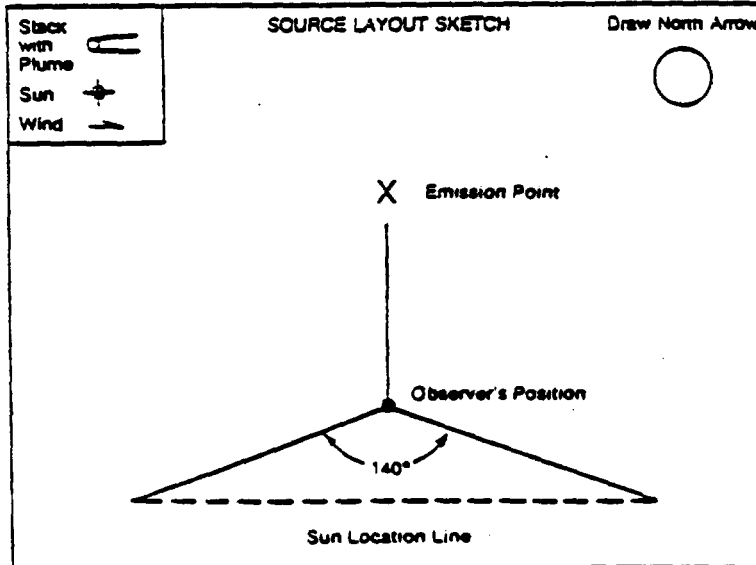
SKY CONDITIONS
Start End

WIND SPEED

WIND DIRECTION
Start End

AMBIENT TEMP

WET BULB TEMP RH, percent
Start End



ADDITIONAL INFORMATION

OBSERVATION DATE <i>6/29/87</i>		START TIME		END TIME	
SEC	0	15	30	45	COMMENTS
1	0	0	0	0	Start 1725
2	0	0	0	0	
3	0	0	0	0	
4	0	0	0	0	
5	0	0	0	0	
6	0	0	0	0	
7	0	0	0	0	
8	0	0	0	0	
9	0	0	0	0	
10	0	0	0	0	
11	0	0	0	0	
12	0	0	0	0	
13	0	0	0	0	
14	0	0	0	0	
15	0	0	0	0	
16	0	0	0	0	
17	0	0	0	0	
18	0	0	0	0	
19	0	0	0	0	
20	0	0	0	0	
21	0	0	0	0	
22	0	0	0	0	
23	0	0	0	0	
24	0	0	0	0	
25	0	0	0	0	
26	0	0	0	0	
27	0	0	0	0	
28	0	0	0	0	
29	0	0	0	0	
30	0	0	0	0	

OBSERVER'S NAME (PRINT)
Michael Kirkman

OBSERVER'S SIGNATURE
Michael Kirkman

DATE
6/29/87

ORGANIZATION
Entropy

CERTIFIED BY

DATE

CONTINUED ON VEO FORM NUMBER
END

VISIBLE EMISSIONS EVALUATOR

This is to certify that

Michael J. Kitzberger

met the specifications of Federal Reference Method 9 and qualified as a visible emissions evaluator. Maximum deviation on white and black smoke did not exceed 7.5% opacity and no single error exceeding 1.5% opacity was incurred during the certification test conducted by Eastern Technical Associates of Raleigh, North Carolina. This certificate is valid for six months from date of issue.

President

Certificate Number

Thomas A. Koe

218134

Vice President

Edna J. Lee

Program Manager

David Savage

May 13 1981

Date of Issue

APPENDIX C

CALIBRATION DATA

QUALITY ASSURANCE PROCEDURES

General. Each item of field test equipment purchased or constructed by Entropy is assigned a unique, permanent identification number. New items for which calibration is required are calibrated before initial field use. Equipment whose calibration status may change with use or with time is inspected in the field before testing begins, and again upon return from each field use. When an item of equipment is found to be out of calibration, it is adjusted and recalibrated or retired from service. All equipment is periodically recalibrated in full, regardless of the outcome of these regular inspections.

Calibrations are conducted in a manner and at a frequency which meet or exceed U. S. EPA specifications. Entropy follows the calibration procedures outlined in EPA Reference Methods, and those recommended within the Quality Assurance Handbook for Air Pollution Measurement Systems: Volume III (EPA-600/4-77-027b, August, 1977). When the Reference Methods are inapplicable, Entropy uses methods such as those prescribed by the American Society for Testing and Materials (ASTM).

Data obtained during calibrations are recorded on standardized forms, which are checked for completeness and accuracy by the Quality Assurance Manager or the Quality Assurance Director. Data reduction and subsequent calculations are performed using Entropy's in-house computer facilities. Calculations are generally performed at least twice as a check for accuracy. Copies of calibration data are included in the test or project reports.

Inspection and Maintenance. An effective preventive maintenance program is necessary to ensure data quality. Each item of equipment returning from the field is inspected before it is returned to storage. During the course of these inspections, items are cleaned, repaired, reconditioned, and recalibrated where necessary.

Each item of equipment transported to the field for this test program was inspected again before being packed. Entropy performs these quality assurance activities prior to departure for the job site to detect equipment problems which may originate during periods of storage. This minimizes lost time on site due to equipment failure.

Occasional equipment failure in the field is unavoidable despite the most rigorous inspection and maintenance procedures. For this reason, Entropy routinely transports sufficient backup equipment to the job site to have complete redundancy of all critical sampling train components.

Calibration. Emissions sampling equipment that requires calibration includes the nozzle, pitot tube, pressure gauges, thermometers, flow meters, dry gas meters, and barometers. The following sections elaborate on the calibration procedures followed by Entropy for these items of equipment. Calibration data for the specific items of equipment used for this test program follow the text.

Nozzles. Each probe nozzle is uniquely and permanently identified at the time of purchase, and calibrated before initial field use. The inside diameter of the nozzle is measured to the nearest 0.001 in. using a micrometer. Five measurements are made using different diameters each time. If the difference between the high and the low numbers does not exceed 0.004 inch, the average of the five measurements is used. If the difference exceeds this amount, or when the nozzle becomes nicked, dented, or corroded, the nozzle is reshaped, sharpened, and recalibrated.

Pitot Tubes. All Type S pitot tubes used by Entropy, whether separate or attached to a sampling probe, are constructed in-house or by Nutech Corporation. Each pitot is calibrated when new in accordance with the geometry standards contained in EPA Reference Method 2. A Type S pitot tube, constructed and positioned according to these standards, will have a coefficient of 0.84 ± 0.02 . This coefficient should not change as long as the pitot tube is not damaged.

Each pitot tube is inspected visually before it is transported to the field. If this inspection indicates damage or raises doubt that the pitot remains in accordance with the EPA geometry standards, the pitot tube is not used until it has been refurbished and recalibrated.

Differential Pressure Gauges. Some meter consoles used by Entropy are equipped with 10 in. W.C. inclined-vertical manometers. Fluid manometers

do not require calibration other than leak checks. Manometers are leak-checked in the field prior to each test series, and again upon return from the field.

Most of Entropy's meter consoles are equipped with Magnehelic differential pressure gauges. Each set of gauges is calibrated initially over its full range, 0-10 inches W.C. After each field use, the calibration of the gauge set is checked against an inclined manometer at the average Δp encountered during the test. If the agreement is within ± 5 percent, the calibration is acceptable.

Thermometers

Impinger Thermometer. On site, prior to the start of testing, the thermometer used to monitor the temperature of the gas leaving the last impinger is compared with a mercury-in-glass thermometer which meets ASTM E-1 specifications. The impinger thermometer is adjusted if necessary until it agrees within 2°F of the reference thermometer. (If the thermometer is not adjustable, it is labeled with a correction factor).

Dry Gas Meter Thermometer. The thermometer used to measure the temperature of the metered gas sample is checked prior to each field trip against an ASTM mercury-in-glass thermometer. The dry gas meter thermometer is acceptable if the values agree with 5.4°F . Thermometers not meeting this requirement are adjusted or labeled with a correction factor.

Flue Gas Temperature Sensor. All thermocouples employed by Entropy for the measurement of flue gas temperatures are calibrated upon receipt. Initial calibrations are performed at three points (ice bath, boiling water, and hot oil). An ASTM mercury-in-glass thermometer is used as a reference. The thermocouple is acceptable if the agreement is within 1.5 percent (absolute) at each of the three calibration points.

On site, prior to the start of testing, the reading from the stack gas thermocouple-potentiometer combination is compared with a mercury-in-glass reference thermometer. If the two agree within 1.5 percent (absolute), the thermocouple and potentiometer are considered to be in proper working order for the test series.

After each field use, the thermocouple-potentiometer system is compared with an ASTM mercury-in-glass reference thermometer at a temperature within 10 percent of the average absolute flue gas temperature. If the absolute temperatures agree within 1.5 percent, the temperature data are considered valid.

Dry Gas Meter and Orifice. The dry gas meter and orifice are calibrated simultaneously. There are two calibration procedures. The full calibration is a complete laboratory procedure used to obtain the calibration factor of the dry gas meter before its first use and periodically thereafter. Full calibrations are performed at three different orifice settings (flow rates). A simpler procedure, the posttest calibration, is designed to check whether the calibration factor has changed. Posttest calibrations are performed after each field test series at an intermediate orifice setting (based on the test data) and at the maximum vacuum reached during the test.

Entropy uses as a transfer standard a dry gas meter that is calibrated annually against a spirometer. During the annual calibration, triplicate calibration runs are performed at seven flow rates ranging from 0.25 to 1.40 cfm.

Dry Gas Meter. Each metering system receives a full calibration at the time of purchase, and a posttest calibration after each field use. If the calibration factor, Y , deviates by less than five percent from the initial value, the test data are acceptable. If Y deviates by more than five percent, the meter is recalibrated and the meter coefficient (initial or recalibrated) that yields the lowest sample volume for the test runs is used.

EPA Reference Method 5 calls for another full calibration anytime the posttest calibration check indicates that Y has changed by more than five percent. Standard practice at Entropy is to recalibrate the dry gas meter anytime Y is found to be outside the range $0.98 \leq Y \leq 1.02$.

Orifice. An orifice calibration factor is calculated for each flow setting during a full calibration. If the range of values does not vary by more than 0.15 in. H_2O over the range of 0.4 to 4.0 in. H_2O , the arithmetic average of the values obtained during the calibration is used.

Barometer. Each field barometer is adjusted before each test series to agree within ± 0.1 inches of a reference aneroid barometer. The reference barometer is checked weekly against the station pressure value (corrected for elevation difference) reported by the National Weather Service station at the Raleigh-Durham airport, approximately 2.5 miles from Entropy's location.

SAMPLING EQUIPMENT CALIBRATION CHECKLIST

JOB NAME/NUMBER Cumberland Paving Co. 536 TEAM LEADER JMS

SAMPLING LOCATION Baghouse Stack

BAROMETER CHECK

DATE	ENTROPY IN-HOUSE REFERENCE BAROMETER	FIELD BAROMETER
6-29-87	29.9	29.9

THERMOMETERS AND THERMOCOUPLE CHECK

DATE	REFERENCE THERMOMETER AMBIENT TEMPERATURE	69 °F			
<table style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="width: 40%;"></th> <th style="width: 30%; text-align: center;"><u>AMBIENT TEMPERATURE °F</u></th> <th style="width: 30%; text-align: center;"><u>MUST BE WITHIN ACCEPTANCE RANGE °F</u></th> </tr> </thead> </table>				<u>AMBIENT TEMPERATURE °F</u>	<u>MUST BE WITHIN ACCEPTANCE RANGE °F</u>
	<u>AMBIENT TEMPERATURE °F</u>	<u>MUST BE WITHIN ACCEPTANCE RANGE °F</u>			
<u>THERMOMETERS</u>					
Impinger Exit	<u>70</u>	<u>+2 °F</u>			
Filter Compartment	<u>67</u>	<u>+5.4 °F</u>			
Dry Gas Meter	<u>69</u>	<u>+5.4 °F</u>			
Other	_____				
<u>THERMOCOUPLE</u>	<u>69</u>	<u>+8 °F</u>			
NOTE: Adjust thermometer until acceptable. If thermometer can't be adjusted, use a backup. If no back up, then record the ambient temperature indicated by the unadjusted thermometer.					

PITOT AND NOZZLE CHECK

PITOTS

I.D.

VISUAL INSPECTION CHECK

4-3

✓

NOZZLES

501

✓

ENTROPY

Dry Gas Meter Identification: 1017051 Calibration by: A. H. H. H. H.

Date: 4-1-66 Barometric Pressure (P_b): 29.86 In. Hg
 Date: Barometric Pressure (P_b): In. Hg

Approx. Flow Rate (Q) cfm	Spirometer		Dry Gas Meter		Pressure (P_p) in. H ₂ O	Time (t) min.	Flow Rate (Q) cfm	Meter Coeff. (V_{ds})	Avg. Meter Coeff. ($\bar{V}_{ds}$)
	Gas Volume (V_g) ft ³	Temp. (T_g) °F	Gas Volume (V_{dg}) ft ³	Temp. (T_{dg}) °F					
0.40	4.062	78.8	4.062	80	0.85	10.0	0.3971	1.0001	
	4.117	79.3	4.061	80	0.85	10.0	0.4021	1.0130	
	4.154	79.7	4.065	80	0.85	10.0	0.4088	1.0289	
	6.084	79.7	6.035	80	1.3	10.0	0.5938	1.0055	
	6.166	79.7	6.016	80	1.275	10.0	0.6018	1.0223	
0.60	6.102	79.7	6.015	80	1.25	10.0	0.5955	1.0119	
	8.051	79.7	7.994	80	2.35	10.0	0.7902	1.0074	
	8.132	79.7	8.003	80	2.40	10.0	0.7937	1.0107	
0.80	8.114	79.3	7.916	80	2.45	10.0	0.7925	1.0100	
	10.128	78.8	10.111	80	3.875	10.0	0.9901	0.9936	
	10.164	78.8	10.081	80	3.80	10.0	0.9936	1.0011	
1.0	10.173	78.8	10.092	80	3.80	10.0	0.9915	1.0009	
	12.359	78.8	12.305	80	5.5	10.0	1.2012	0.9932	
	12.368	78.8	12.316	80	5.3	10.0	1.2051	0.9935	
1.2	12.313	78.8	12.274	80	5.3	10.0	1.2031	0.9925	

$$V_{ds} = \frac{(V_g)(L_{ds} + 460)(P_b)}{(V_{dg})(T_g + 460)(P_b) + (P - P_b)(T_g + 460)}$$

$$Q = (17.64) \frac{(P_b)(V_g)}{(P - P_b)(T_g + 460)}$$

Calibration by:

Barometric Pressure (P_b): 29.86 In. Hg

9.8.52

Dale:

ENTROPY
ENVIRONMENTAL BILLING

Date:

Barometric Pressure (r_b): _____ in. Hg[illegible]

$$Y_{DS} = \frac{(V_S)(t_{DS} + t_{b})}{(V_{DS} + V_{b})(t_{DS} + t_{b})}$$

$$Q = (17.61) \frac{(V_b)(V_s)}{(V_s + 460)(3)}$$

Meter Box Number: N4

Calibration by: T. McDonald

Standard Meter Number: 1017057 Standard Meter Gamma: 1.002

Date: 3/27/87 Barometric Pressure (P_b): 29.42 in. Hg

*Date: _____ *Barometric Pressure (P_b): _____ in. Hg

PRETEST CALIBRATION

Standard Meter			Meter Box Metering System				
Gas Volume (V_{ds}) ft ³	Temp. (t_{ds}) °F	Time (θ) min.	Orifice Setting (ΔH) in. H ₂ O	Gas Volume (V_d) ft ³	Temp. (t_d) °F	Coeff. (Y_d)	ΔH_e in. H ₂ O
4.002	69	10.0	0.50	4.082	73	0.9886	1.759
4.114	69	10.0	0.50	4.211	75	0.9881	1.661
8.182	69	10.0	2.1	8.323	79	0.9984	1.748
8.177	69	10.0	2.1	8.350	82 82	1.0001	1.74
12.168	69	10.0	4.8	12.355	84	1.0028	1.79
12.127	69	10.0	4.8	12.341	87	1.0061	1.79
Average						0.9974	1.75

2.997

$$Y_d = \frac{Y_{ds} * V_{ds} * (t_d + 460) * P_b}{V_d * (t_{ds} + 460) * (P_b + H/13.6)}$$

$$\Delta H_e = \frac{0.0317 * \Delta H}{P_b * (t_d + 460)} * \left[\frac{(t_{ds} + 460) * \theta}{Y_{ds} * V_{ds}} \right]^2$$

Meter Box Number: N4Calibration by: T. MS DonaldMeter Box Vacuum: 6 in. HgStandard Meter Number: 1017057 Standard Meter Gamma: 1.002Date: 7/1/87 Barometric Pressure (P_b): 29.57 in. HgPOSTTEST CALIBRATION

Standard Meter			Meter Box Metering System				
Gas Volume (V_{ds}) ft ³	Temp. (t_{ds}) °F	Time (θ) min.	Orifice Setting (ΔH) in. H ₂ O	Gas Volume (V_d) ft ³	Temp. (t_d) °F	Coeff. (Y_d)	ΔH_e in. H ₂ O
6.468	74	10.0	1.25	6.309	78	1.0000	1.69
6.432	74	10.0	1.25	6.499	81	1.0016	1.70
6.392	74	10.0	1.25	6.503	84	1.0002	1.71
Average						1.0006	1.70

$$Y_d = \frac{Y_{ds} * V_{ds} * (t_d + 460) * P_b}{V_d * (t_{ds} + 460) * (P_b + \Delta H/13.6)}$$

$$\Delta H_e = \frac{0.0317 * \Delta H}{P_b * (t_d + 460)} * \left[\frac{(t_{ds} + 460) * \theta}{Y_{ds} * V_{ds}} \right]^2$$

NOZZLE NUMBER: 501

[illegible]

NOTE: All diameters measured in inches.

APPENDIX D

SAMPLING AND ANALYTICAL PROCEDURES