

Note: This is a reference cited in AP 42, *Compilation of Air Pollutant Emission Factors, Volume I Stationary Point and Area Sources*. AP42 is located on the EPA web site at [www.epa.gov/ttn/chief/ap42/](http://www.epa.gov/ttn/chief/ap42/)

The file name refers to the reference number, the AP42 chapter and section. The file name "ref02\_c01s02.pdf" would mean the reference is from AP42 chapter 1 section 2. The reference may be from a previous version of the section and no longer cited. The primary source should always be checked.

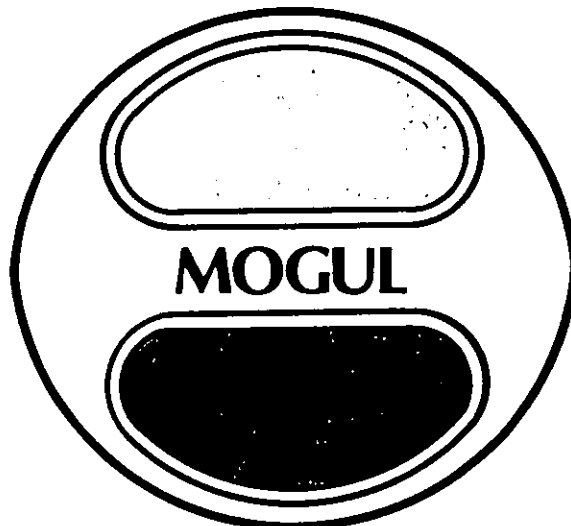
|                    |                                                                                                                                           |
|--------------------|-------------------------------------------------------------------------------------------------------------------------------------------|
| AP42 Section:      | 11.3                                                                                                                                      |
| Background Chapter | 4                                                                                                                                         |
| Reference:         | 18                                                                                                                                        |
| Title:             | <i>Particulate Compliance Analysis For<br/>The Coal-Fired Brick Kiln, The Mogul<br/>Corporation, Charlotte,<br/>NC, January 24, 1978.</i> |

AP-42 Section 11.3  
Reference NOT USED  
Report Sect. 4  
Reference 1B

Sect. 9, Ref 1B

ONLY  
1  
Run!

# MOGUL **enviro**service™



ENVIRONMENTAL CONTROL SERVICES

THE MOGUL CORPORATION



# The Mogul Corporation

WATER TREATMENT PRODUCTS AND SERVICES SINCE 1915  
CHAGRIN FALLS, OHIO 44022 (216) 247-5000 TELEX NUMBER 98-0324

REPLY TO:

Southern Division  
1201 S. Graham Street  
Charlotte, North Carolina 28203  
(704) 375-5726

February 13, 1978

Mr. Paul Sieffert  
Pullman-Swindell  
441 Smithfield St.  
Pittsburg, Pa. 15222

Subject: Particulate Compliance Testing

Dear Mr. Sieffert:

Enclosed are the results of the particulate compliance testing performed on the brick kiln at the Lee Brick and Tile plant, Sanford, N. C. on January 24, 1978.

If you should have questions which are not answered by this report, please do not hesitate to contact me at our Charlotte office.

Thank you very much for utilizing Mogul's EnviroServices program to obtain your particulate emission rates.

Yours very truly,

THE MOGUL CORPORATION

*W. D. Fink*  
W. D. Fink  
Laboratory Manager

WDF/bc

cc: In triplicate  
Mr. Owen Foster  
Mr. Bill McConnell

Enclosures

RECEIVED

FEB 22 1978

AIR QUALITY DIVISION  
CENTRAL OFFICE

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AUSTRALIA  
The Nightingale Supply Co., Ltd.  
Sydney, N. S. W.

PREPARED ESPECIALLY FOR:

PULLMAN-SWINDELL  
LEE BRICK AND TILE PLANT  
SANFORD, N. C.

TESTS: Particulate Compliance Analysis  
for the Cold Fired Brick Kiln

TESTS CONDUCTED BY: The Mogul Corporation  
Mr. R. M. Pearce, Team Leader  
Mr. Lewis Frederick, Assistant

TEST DATE: January 24, 1978

REPORT NUMBER: S-12277-1

REPORT BY: R. M. Pearce

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## INTRODUCTION

Particulate sampling of the stack gases emitted from the cold fired brick kiln was performed at the Lee Brick and Tile plant, Sanford, N. C. on January 24, 1978.

One two hour test was performed on each of the two stacks to determine the pollutant mass rate according to the regulations of the State of North Carolina. There were no observers from the State of North Carolina present.

## SAMPLING AND ANALYTICAL PROCEDURES

These sources were tested utilizing a Nutech Corporation, model 201-300 particulate stack sampling system, which meets the designed specification of the Environmental Protection Agency. The method utilized for particulate analysis was the Environmental Protection Agency method as presented in the Federal Register Volume 42, 160, August 8, 1977, Method V "Determination of Particulate Emissions for Stationary Sources".

## RESULTS

For ease of interpretation, the attached tables outline the results of each test performed. The computerized calculations and raw data sheets have been included in the report for specific calculation information.

## DISCUSSION

The maximum allowable emission rate in lbs./hr. of process was taken from the Rules and Regulations Governing the Control of Air Pollution, Board of Water and Air Resources, Raleigh, N. C., January 21, 1972, page c-30, c-31.

SUMMARY OF RESULTS

| <u>RUN NUMBER</u> | <u>TONS OF PROCESS<br/>PER HOUR</u> | <u>EMISSION RATE<br/>LBS./HR.</u> | <u>% ISOKINETIC</u> | <u>ALLOWABLE EMISSION<br/>RATE LBS./HR</u> |
|-------------------|-------------------------------------|-----------------------------------|---------------------|--------------------------------------------|
| 1                 | 10.37                               | 11.95                             | 103.28              | 9.9                                        |
| 2                 | 10.37                               | 27.85                             | 101.36              | 9.9                                        |
|                   |                                     |                                   |                     |                                            |
|                   | TOTAL                               | 39.80                             | TOTAL               | 19.8                                       |

101 % over

JOB NUMBER 800122  
CLIENT NUMBER 100TH

01/21/78.  
STACK LOCATION PRICEHILL

SUMMARY OF STACK TESTING RESULTS - PROCESS

PAGE 1

RUN NUMBER AND DATE  
1  
1/24/78

|                                                                           |        |
|---------------------------------------------------------------------------|--------|
| AVERAGE STACK VELOCITY, FPM (VSD)                                         | 1106.  |
| ACTUAL STACK FLOW RATE, CFPM (VDA)                                        | 7816.  |
| STACK FLOW RATE, DRY, STD. COND.,<br>CFM (VSD)                            | 4210.  |
| AVERAGE STACK TEMPERATURE, F (TSD)                                        | 478.   |
| STACK GAS VELOCITY HEAD, IN. H <sub>2</sub> O (DELP)                      | .059   |
| PERCENT ISOCHINETIC (IARD)                                                | 103.28 |
| PARTICULATE COLLECTED, MG<br>PROBE, CYCLONE AND FILTER (WARD)             | 2178.9 |
| IMPINGERS (WARD)                                                          | N/A    |
| TOTAL (WARD)                                                              | 2178.9 |
| PARTICULATE EMISSION, POUNDS PER HOUR<br>PROBE, CYCLONE AND FILTER (WARD) | 11.95  |
| IMPINGERS (WARD)                                                          | N/A    |
| TOTAL (WARD)                                                              | 11.95  |
| PARTICULATE CONC., GRAINS PER DCF<br>PROBE, CYCLONE AND FILTER (WARD)     | .3309  |
| IMPINGERS (WARD)                                                          | N/A    |
| TOTAL (WARD)                                                              | .3309  |
| PRODUCTION WEIGHT, TONS PER HOUR (WTD)                                    | 10.37  |

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JOB NUMBER 800122  
CLIENT NUMBER 100TH

01/31/78.  
STACK LOCATION BR1011LN

SUMMARY OF STACK TESTING RESULTS - PROCESS

PAGE 2

RUN NUMBER AND DATE

1  
1/24/78

|                                                                  |         |
|------------------------------------------------------------------|---------|
| STACK AREA, SQUARE INCHES (A)                                    | 1017.88 |
| BAROMETRIC PRESSURE, INCHES HG (PBAR)                            | 29.40   |
| GAUGE PRESSURE OF STACK GAS, INCHES<br>HG (PG)                   | N/D     |
| STACK PRESSURE (ABS.), INCHES HG (PS)                            | 29.40   |
| AVERAGE ORIFICE PRESSURE DROP,<br>INCHES WATER (DELTA)           | 2.3     |
| NET TIME OF TEST, MINUTES (THETA)                                | 120.    |
| SAMPLING NOZZLE DIAMETER INCHES (AND)                            | .500    |
| AVERAGE METER TEMPERATURE, F (TM)                                | 71.     |
| VOLUME OF DRY GAS SAMPLED AT METER<br>CONDITIONS, CF (VM)        | 102.48  |
| VOLUME OF DRY GAS SAMPLED AT<br>STANDARD CONDITIONS, SCF (VMSTD) | 101.59  |
| TOTAL WATER COLLECTED IN IMPINGERS<br>AND SILICA GEL, GM (VLC)   | 58.2    |
| VOLUME OF WATER VAPOR AT STANDARD<br>CONDITIONS, CF (VMSTD)      | 2.74    |

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UNIT NUMBER 200122  
CLIENT NUMBER 200TH

01/31/78.  
STACK, LOCATION BRICK LUM

SUMMARY OF STACK TESTING RESULTS - PROCESS

PAGE 3

RUN NUMBER AND DATE  
1  
1/24/78

|                                               |       |
|-----------------------------------------------|-------|
| PERCENT MOISTURE BY VOLUME (BMS)              | 2.63  |
| MOLE FRACTION OF DRY GAS (MCH)                | .97   |
| PERCENT CO <sub>2</sub> BY VOLUME, DRY (VBFD) | 5.0   |
| PERCENT CO BY VOLUME, DRY (VBGS)              | N/D   |
| PERCENT O <sub>2</sub> BY VOLUME, DRY (VBHD)  | 16.0  |
| PERCENT N <sub>2</sub> BY VOLUME, DRY (VBID)  | 79.0  |
| MOLECULAR WEIGHT, DRY STACK GAS (MD)          | 29.44 |
| MOLECULAR WEIGHT, NET BASIS (MS)              | 29.14 |
| PITOT TUBE COEFFICIENT (CP)                   | .85   |
| DRY GAS METER CALIBRATION FACTOR (C)          | 1.01  |
| NET SAMPLING POINTS (ND)                      | 48    |

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N/D = NOT DETECTED

JOB NUMBER 800123  
CLIENT NUMBER 500TH

01/31/78.  
STACK LOCATION BRIDGEHILL

SUMMARY OF STACK TESTING RESULTS - PROCESS

PAGE 4

RUN NUMBER AND DATE

82  
1/24/78

|                                                                          |        |
|--------------------------------------------------------------------------|--------|
| AVERAGE STACK VELOCITY, FPM (VS)                                         | 4454.  |
| ACTUAL STACK FLOW RATE, CFPM (VDR)                                       | 31486. |
| STACK FLOW RATE, DRY, STD. COND.,<br>CFM (CSD)                           | 23197. |
| AVERAGE STACK TEMPERATURE, F (TS)                                        | 239.   |
| STACK GAS VELOCITY HEAD, IN. H <sub>2</sub> O (DELP)                     | 1.269  |
| PERCENT ISOKINETIC (IAX)                                                 | 101.36 |
| PARTICULATE COLLECTED, MG,<br>PROBE, CYCLONE AND FILTER (MAK)            | 701.1  |
| IMPINGERS (VAL)                                                          | N/A    |
| TOTAL (MAL)                                                              | 701.1  |
| PARTICULATE EMISSION, POUNDS PER HOUR<br>PROBE, CYCLONE AND FILTER (CAN) | 27.85  |
| IMPINGERS (BAV)                                                          | N/A    |
| TOTAL (CAX)                                                              | 27.85  |
| PARTICULATE CONC., GRAINS PER DSCF<br>PROBE, CYCLONE AND FILTER (CAN)    | .1400  |
| IMPINGERS (BAM)                                                          | N/A    |
| TOTAL (CAR)                                                              | .1400  |
| PRODUCTION WEIGHT, TONS PER HOUR (WIT)                                   | 10.37  |

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JOB NUMBER 800123  
CLIENT NUMBER 50014

01/31/78.  
STACK LOCATION BRICKFIELD

SUMMARY OF STACK TESTING RESULTS - PROCESS

PAGE 5

RUN NUMBER AND DATE  
X 2  
1/24/78

|                                                                  |         |
|------------------------------------------------------------------|---------|
| STACK AREA, SQUARE INCHES (A)                                    | 1017.88 |
| BAROMETRIC PRESSURE, INCHES HG (PBAR)                            | 29.36   |
| GAUGE PRESSURE OF STACK GAS, INCHES<br>HG (PG)                   | N/D     |
| STACK PRESSURE (ABS.), INCHES HG (PS)                            | 29.36   |
| AVERAGE ORIFICE PRESSURE DROP,<br>INCHES WATER (DELTA)           | 1.3     |
| NET TIME OF TEST, MINUTES (THETA)                                | 120.    |
| SAMPLING NOZZLE DIAMETER, INCHES (AND)                           | .188    |
| AVERAGE METER TEMPERATURE, F (TM)                                | 82.     |
| VOLUME OF DRY GAS SAMPLED AT METER<br>CONDITIONS, CF (VM)        | 79.76   |
| VOLUME OF DRY GAS SAMPLED AT<br>STANDARD CONDITIONS, SCF (VMSTD) | 77.27   |
| TOTAL WATER COLLECTED IN IMPINGERS<br>AND SILICA GEL, GM (WLO)   | 10.1    |
| VOLUME OF WATER VAPOR AT STANDARD<br>CONDITIONS, CF (VMSTD)      | .48     |

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JOB NUMBER 800123  
CLIENT NUMBER SOUTH

01/31/78.  
STACK LOCATION BRICKFIELD

SUMMARY OF STACK TESTING RESULTS - PROCESS

PAGE 6

RUN NUMBER AND DATE

1  
1/24/78

|                                               |       |
|-----------------------------------------------|-------|
| PERCENT MOISTURE BY VOLUME (BWS)              | .61   |
| MOLE FRACTION OF DRY GAS (MDH)                | .99   |
| PERCENT CO <sub>2</sub> BY VOLUME, DRY (VBFD) | 1.5   |
| PERCENT CO BY VOLUME, DRY (VBGD)              | N/D   |
| PERCENT O <sub>2</sub> BY VOLUME, DRY (VBHD)  | 19.5  |
| PERCENT N <sub>2</sub> BY VOLUME, DRY (VBID)  | 79.0  |
| MOLECULAR WEIGHT, DRY STACK GAS (MD)          | 29.02 |
| MOLECULAR WEIGHT, WET BASIS (MS)              | 28.95 |
| PITOT TUBE COEFFICIENT (CP)                   | .85   |
| DRY GAS METER CALIBRATION FACTOR (CY)         | 1.01  |
| NET SAMPLING POINTS (N)                       | 48    |

PREPARED BY THE MOBIL CORPORATION

## Title 40—Protection of Environment

CHAPTER 1—ENVIRONMENTAL  
PROTECTION AGENCY

(PRI, 754-6)

PART 60—STANDARDS OF PERFORMANCE  
FOR NEW STATIONARY SOURCES

## Revision to Reference Methods 1-8

AGENCY: Environmental Protection  
Agency.

ACTION: Final Rule.

**SUMMARY:** This rule revises Reference Methods 1 through 8, the detailed requirements used to measure emissions from affected facilities to determine whether they are in compliance with a standard of performance. The methods were originally promulgated December 23, 1971, and since that time several revisions became apparent which would clarify, correct and improve the methods. These revisions make the methods easier to use, and improve their accuracy and reliability.

**EFFECTIVE DATE:** September 19, 1977.

**ADDRESSES:** Copies of the comment letters are available for public inspection and copying at the U.S. Environmental Protection Agency, Public Information Reference Unit (EPA Library), Room 2922, 401 M Street, S.W., Washington, D.C. 20460. A summary of the comments and EPA's responses may be obtained upon written request from the EPA Public Information Center (PM-215), 401 M Street, S.W., Washington, D.C. 20460 (specify "Public Comment Summary: Revisions to Reference Methods 1-8 in Appendix A of Standards of Performance for New Stationary Sources").

**FOR FURTHER INFORMATION CONTACT:**

Don R. Goodwin, Emission Standards and Engineering Division, Environmental Protection Agency, Research Triangle Park, North Carolina 27711, telephone No. 919-541-5271.

**SUPPLEMENTARY INFORMATION:** The amendments were proposed on June 8, 1976 (40 FR 23060). A total of 55 comment letters were received during the comment period—34 from industry, 15 from governmental agencies, and 6 from other interested parties. They contained numerous suggestions which were incorporated in the final revisions.

Changes common to all eight of the reference methods are: (1) the clarification of procedures and equipment specifications resulting from the comments, (2) the addition of guidelines for alternative procedures and equipment to make prior approval of the Administrator unnecessary and (3) the addition of an introduction to each reference method discussing the general use of the method and delineating the procedure for using alternative methods and equipment.

Specific changes to the methods are:

**METHOD 1**

1. The provision for the use of more than two traverse diameters, when specified by the Administrator, has been deleted. If one traverse diameter is in a plane containing the greatest expected concentration variation, the intended purpose of the deleted paragraph will be fulfilled.

2. Based on recent data from Fluidyne (Particulate Sampling Strategies for Large Power Plants Including Nonuniform Flow, EPA-600/2-76-170, June 1976) and Entropy Environmentalists (Determination of the Optimum Number of Traverse Points: An Analysis of Method 1 Criteria (draft), Contract No. 68-01-3172), the number of traverse points for velocity measurements has been reduced and the 2:1 length to width ratio requirement for cross-sectional layout of rectangular ducts has been replaced by a "balanced matrix" scheme.

3. Guidelines for sampling in stacks containing cyclonic flow and stacks smaller than about 0.31 meter in diameter or 0.071 m<sup>2</sup> in cross-sectional area will be published at a later date.

4. Clarification has been made as to when a check for cyclonic flow is necessary; also, the suggested procedure for determination of unacceptable flow conditions has been revised.

**METHOD 2**

1. The calibration of certain pitot tubes has been made optional. Appropriate construction and application guidelines have been included.

2. A detailed calibration procedure for temperature gauges has been included.

3. A leak check procedure for pitot lines has been included.

**METHOD 3**

1. The applicability of the method has been confined to fossil-fuel combustion processes and to other processes where it has been determined that components other than O<sub>2</sub>, CO<sub>2</sub>, CO, and N<sub>2</sub> are not present in concentrations sufficient to affect the final results.

2. Based on recent research information (Particulate Sampling Strategies for Large Power Plants Including Nonuniform Flow, EPA-600/2-76-170, June 1976), the requirement for proportional sampling has been dropped and replaced with the requirement for constant rate sampling. Proportional and constant rate sampling have been found to give essentially the same result.

3. The "three consecutive" requirement has been replaced by "any three" for the determination of molecular weight, CO, and O<sub>2</sub>.

4. The equation for excess air has been revised to account for the presence of CO.

5. A clearer distinction has been made between molecular weight determination and emission rate correction factor determination.

6. Single point, integrated sampling has been included.

**METHOD 4**

1. The sampling time of 1 hour has been changed to a total sampling time which will span the length of time the pollutant emission rate is being determined or such time as specified in an applicable subpart of the standards.

2. The requirement for proportional sampling has been dropped and replaced with the requirement for constant rate sampling.

3. The leak check before the test run has been made optional; the leak check after the run remains mandatory.

**METHOD 5**

1. The following alternatives have been included in the method:

a. The use of metal probe liners.  
b. The use of other materials of construction for filter holders and probe liner parts.

c. The use of polyethylene wash bottles and sample storage containers.

d. The use of desiccants other than silica gel or calcium sulfate, when appropriate.

e. The use of stopcock grease other than silicone grease, when appropriate.

f. The drying of filters and probe-filter catches at elevated temperatures, when appropriate.

g. The combining of the filter and probe washes into one container.

2. The leak check prior to a test run has been made optional. The post-test leak check remains mandatory. A method for correcting sample volume for excessive leakage rates has been included.

3. Detailed leak check and calibration procedures for the metering system have been included.

**METHOD 6**

1. Possible interfering agents of the method have been delineated.

2. The options of: (a) using a Method 8 Impinger system, or (b) determining SO<sub>2</sub> simultaneously with particulate matter, have been included in the method.

3. Based on recent research data, the requirement for proportional sampling has been dropped and replaced with the requirement for constant rate sampling.

4. Tests have shown that isopropanol obtained from commercial sources occasionally has peroxide impurities that will cause erroneously low SO<sub>2</sub> measurements. Therefore, a test for detecting peroxides in isopropanol has been included in the method.

5. The leak check before the test run has been made optional; the leak check after the run remains mandatory.

6. A detailed calibration procedure for the metering system has been included in the method.

**METHOD 7**

1. For variable wave length spectrophotometers, a scanning procedure for determining the point of maximum absorbance has been incorporated as an option.

**METHOD 8**

1. Known interfering compounds have been listed to avoid misapplication of the method.

2. The determination of filterable particulate matter (including acid mist) simultaneously with SO<sub>2</sub> and SO<sub>3</sub> has been allowed where applicable.

3. Since occasionally some commercially available quantities of isopropanol

have peroxide impurities that will cause erroneously high sulfuric acid mist measurements, a test for peroxides in isopropanol has been included in the method.

4. The gravimetric technique for moisture content (rather than volumetric) has been specified because a mixture of isopropyl alcohol and water will have a volume less than the sum of the volumes of its content.

5. A closer correspondence has been made between similar parts of Methods 8 and 5.

#### MISCELLANEOUS

Several commenters questioned the meaning of the term "subject to the approval of the Administrator" in relation to using alternate test methods and procedures. As defined in § 60.2 of subpart A, the "Administrator" includes any authorized representative of the Administrator of the Environmental Protection Agency. Authorized representatives are EPA officials in EPA Regional Offices or State, local, and regional governmental officials who have been delegated the responsibility of enforcing regulations under 40 CFR 60. These officials in consultation with other staff members familiar with technical aspects of source testing will render decisions regarding acceptable alternate test procedures.

In accordance with section 117 of the Act, publication of these methods was preceded by consultation with appropriate advisory committees, independent experts, and Federal departments and agencies.

(Secs. 111, 114 and 301(a) of the Clean Air Act, sec. 4(a) of Pub. L. No. 91-604, 84 Stat. 1683; sec. 4(a) of Pub. L. No. 91-604, 84 Stat. 1687; sec. 2 of Pub. L. No. 90-148, 81 Stat. 504 [42 U.S.C. 1857c-6, 1857c-9, 1857g(a)].)

**NOTE.**—The Environmental Protection Agency has determined that this document does not contain a major proposal requiring preparation of an Economic Impact Analysis under Executive Orders 11821 and 11949 and OMB Circular A-107.

Dated: August 10, 1977.

DOUGLAS M. COSTLE,  
Administrator.

Part 60 of Chapter I of Title 40 of the Code of Federal Regulations is amended by revising Methods 1 through 8 of Appendix A—Reference Methods as follows:

#### APPENDIX A—REFERENCE METHODS

The reference methods in this Appendix are referred to in § 60.8 (Performance Tests) and § 60.13 (Compliance With Standards and Maintenance Requirements) of 40 CFR Part 60, Subpart A (General Provisions). Specific uses of these reference methods are described in the standards of performance contained in the subparts, beginning with Subpart D.

Within each standard of performance, a section titled "Test Methods and Procedures" is provided to (1) identify the test method applicable to the facility subject to the respective standard and (2) identify any special instructions or conditions to be followed when applying a method to the respective facility. Such instructions (for example, establish sampling rates, volumes, or temperatures) are to be used either in addition to, or as a substitute for, procedures in a reference method. Similarly, for sources subject to emission monitoring requirements, specific instructions pertaining to any use of a reference method are provided in the subpart or in Appendix B.

Inclusion of methods in this Appendix is not intended as an endorsement or denial of their applicability to sources that are not subject to standards of performance. The methods are potentially applicable to other sources; however, applicability should be confirmed by careful and appropriate evaluation of the conditions prevalent at such sources.

The approach followed in the formulation of the reference methods involves specifications for equipment, procedures, and performance. In many cases, a performance specification approach would be preferable in all methods because this allows the greatest flexibility to the user. In parallel, however, this approach is impractical in most cases because performance specifications cannot be established. Most of the methods described herein, therefore, involve specific equipment specifications and procedures, and only a few methods in this Appendix rely on performance criteria.

Minor changes in the reference methods should not necessarily affect the validity of the results and it is recognized that alternative and equivalent methods exist. Section 60.8 provides authority for the Administrator to specify or approve (1) equivalent methods, (2) alternative methods, and (3) minor changes in the nomenclature of the reference methods. It should be clearly understood that unless otherwise identified all such methods and changes must have prior approval of the Administrator. An owner employing such methods or deviations from the reference methods without obtaining prior approval does so at the risk of subsequent disapproval and retesting with approved methods.

Within the reference methods, certain specific equipment or procedures are recognized as being acceptable or potentially acceptable and are specifically identified in the methods. The items identified as acceptable options may be used without approval but must be identified in the test report. The potentially acceptable options are cited as "subject to the approval of the Administrator" or as "or equivalent." Such potentially acceptable techniques or alternatives may be used at the discretion of the owner without prior approval. However, detailed descriptions for applying these potentially acceptable techniques or alternatives are not provided in the reference methods. Also, the potentially acceptable options are not necessarily acceptable in all applications. Therefore, an owner electing to use such potentially acceptable techniques or alternatives is responsible for: (1) assuring that the techniques or alternatives are in fact applicable and are properly executed; (2) including a written description of the alternative method in the test report (the written method must be clear and must be capable of being performed without additional instruction, and the degree of detail should be similar to the detail contained in the reference methods); and (3) providing any rationale or supporting data necessary to show the validity of the alternative in the particular application. Failure to meet these requirements can result in the Administrator's disapproval of the alternative.

#### METHOD 1 SAMPLE AND VELOCITY TRAVERSERS FOR STATIONARY SOURCES

##### 1. Principle and Applicability

1.1 Principle. To aid in the representative measurement of pollutant emissions and/or total volumetric flow rate from a stationary source, a measurement site where the effluent stream is flowing in a known direction is selected, and the cross-section of the stack is divided into a number of equal areas. A traverse point is then located within each of these equal areas.

1.2 Applicability. This method is applicable to flowing gas streams in ducts, stacks, and flues. The method cannot be used when: (1) flow is cyclonic or swirling (see section 2.4); (2) a stack is smaller than about 0.30 meter (12 in.) in diameter, or 0.051 m<sup>2</sup> (13 in.<sup>2</sup>) in cross-sectional area; or (3) the measurement site is less than two stack or duct diameters downstream or less than a half diameter upstream from a flow disturbance.

The requirements of this method must be considered before construction of a new facility from which emissions will be measured; failure to do so may require subsequent alterations to the stack or deviation from the standard procedure. Cases involving variants are subject to approval by the Administrator, U.S. Environmental Protection Agency.

##### 2. Procedure

2.1 Selection of Measurement Site. Sampling or velocity measurement is performed at a site located at least eight stack or duct diameters downstream and two diameters upstream from any flow disturbance such as a bend, expansion, or contraction in the stack, or from a visible flame. If necessary, an alternative location may be selected, at a position at least two stack or duct diameters downstream and a half diameter upstream from any flow disturbance. For a rectangular cross section, an equivalent diameter ( $D_e$ ) shall be calculated from the following equation, to determine the upstream and downstream distances:

$$D_e = \frac{2LW}{L+W}$$

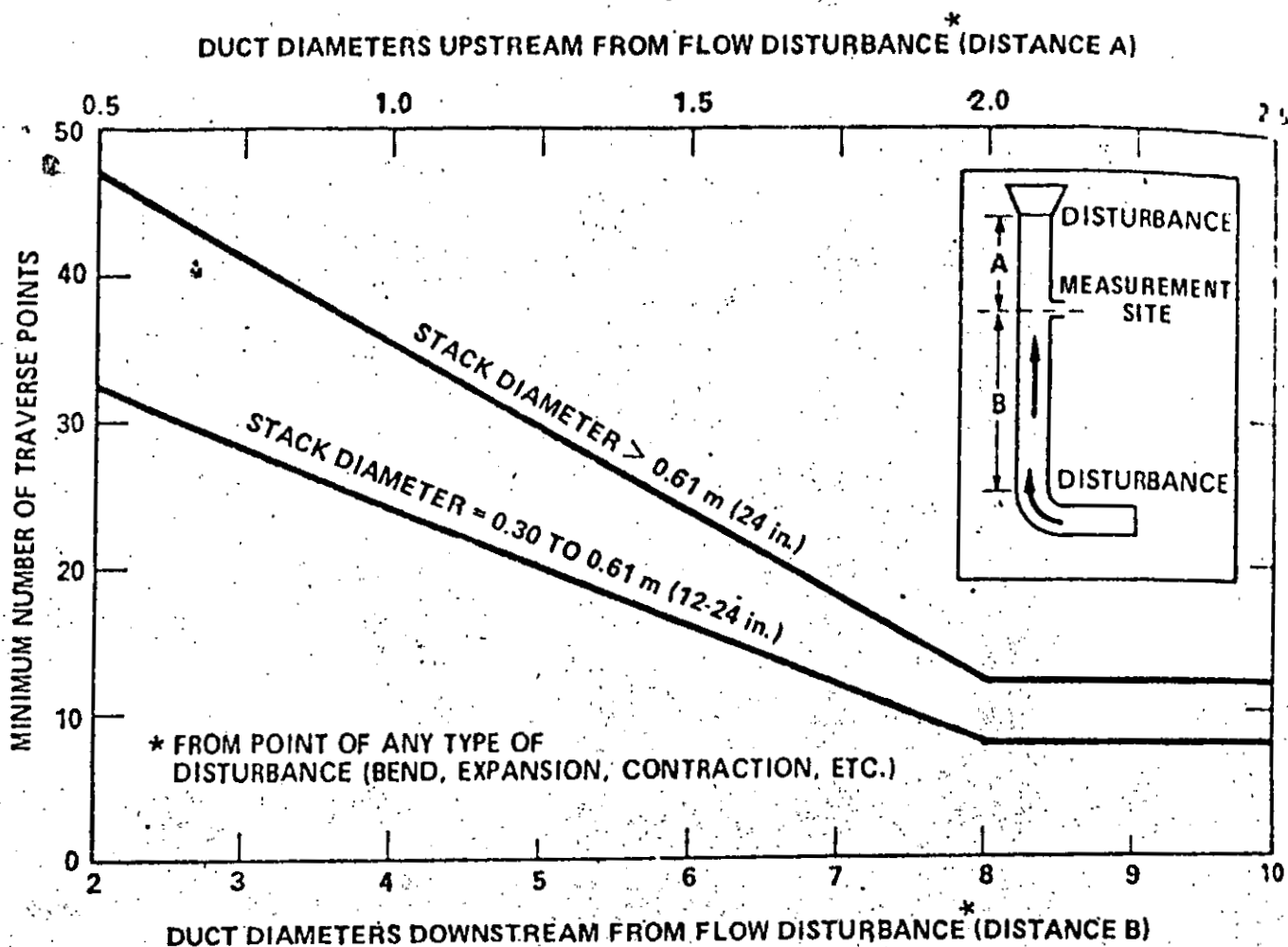


Figure 1-1. Minimum number of traverse points for particulate traverses.

where  $L$  = length and  $W$  = width.

2.2. Determining the Number of Traverse Points.

2.2.1. Particulate Traverses. When the eight- and two-diameter criterion can be met, the minimum number of traverse points shall be: (1) twelve, for circular or rectangular stacks with diameters (or equivalent diameters) greater than 0.61 meter (24 in.); (2) eight, for circular stacks with diameters between 0.30 and 0.61 meter (12-24 in.); (3) nine, for rectangular stacks with equivalent diameters between 0.30 and 0.61 meter (12-24 in.).

When the eight- and two-diameter criterion cannot be met, the minimum number of traverse points is determined from Figure 1-1. Before referring to the figure, however, determine the distances from the chosen measurement site to the nearest upstream and downstream disturbances, and divide each distance by the stack diameter or equivalent diameter, to determine the distance in terms of the number of duct diameters. Then, determine from Figure 1-1 the minimum number of traverse points that corresponds: (1) to the number of duct diameters upstream; and (2) to the number of diameters downstream. Select the higher of the two minimum numbers of traverse points, or a greater value, so that for circular stacks the number is a multiple of 4, and for rectangular stacks, the number is one of those shown in Table 1-1.

TABLE 1-1. Cross-sectional layout for rectangular stacks

| Number of traverse points: | Matrix layout |
|----------------------------|---------------|
| 8                          | 3x3           |
| 12                         | 4x3           |
| 16                         | 4x4           |
| 20                         | 5x4           |
| 25                         | 5x5           |
| 30                         | 6x5           |
| 36                         | 6x6           |
| 40                         | 7x6           |
| 48                         | 7x7           |



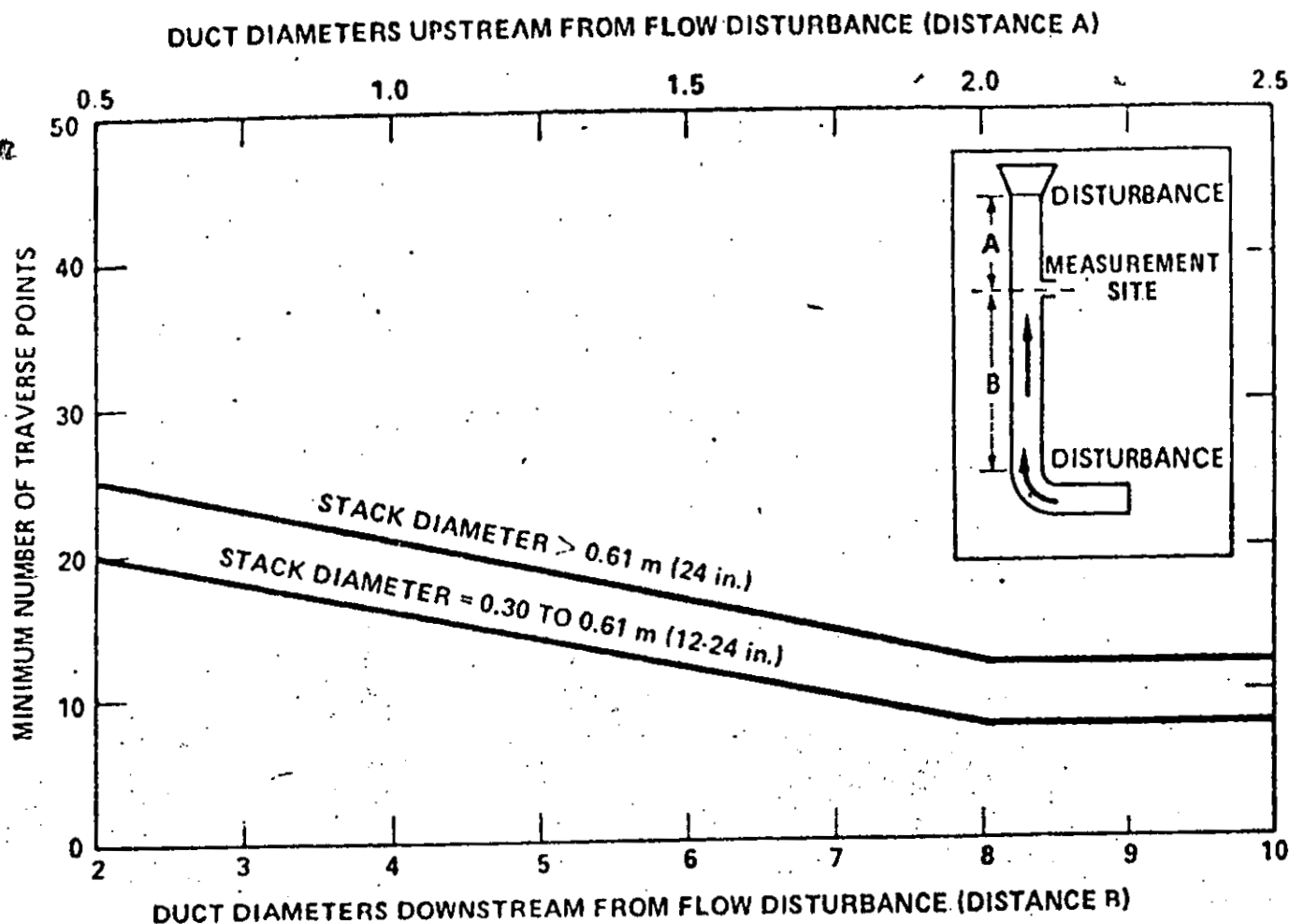


Figure 1-2. Minimum number of traverse points for velocity (nonparticulate) traverses.

2.2.2 Velocity (Non-Particulate) Traverses. When velocity or volumetric flow rate is to be determined (but not particulate matter), the same procedure as that for particulate traverses (Section 2.2.1) is followed, except that Figure 1-2 may be used instead of Figure 1-1.

2.3 Cross-Sectional Layout and Location of Traverse Points.

2.3.1 Circular Stacks. Locate the traverse points on two perpendicular diameters according to Table 1-2 and the example shown in Figure 1-3. Any equation (for example, see Citations 2 and 3 in the Bibliography) that gives the same values as those in Table 1-2 may be used in lieu of Table 1-2.

For particulate traverses, one of the diameters must be in a plane containing the greatest expected concentration variation, e.g., after bends, one diameter shall be in the plane of the bend. This requirement becomes less critical as the distance from the disturbance increases; therefore, other diameters may be used, subject to approval of the Administrator.

In addition, for stacks having diameters greater than 0.61 m (24 in.) no traverse points shall be located within 2.5 centimeters (1.0 in.) of the stack walls; and for stack diameters equal to or less than 0.61 m (24 in.), no traverse points shall be located within 1.3 cm (0.50 in.) of the stack walls. To meet these criteria, observe the procedures given below.

2.3.1.1 Stacks With Diameters Greater Than 0.61 m (24 in.). When any of the traverse points as located in Section 2.3.1 fall within 2.5 cm (1.0 in.) of the stack walls, relocate them away from the stack walls to: (1) a distance of 2.5 cm (1.0 in.); or (2) a distance equal to the nozzle inside diameter, whichever is larger. These relocated traverse points (on each end of a diameter) shall be the "adjusted" traverse points.

Whenever two successive traverse points are combined to form a single adjusted traverse point, treat the adjusted point as two separate traverse points, both in the sampling (or velocity measurement) procedure, and in recording the data.

| TRAVERSE POINT | DISTANCE, % of diameter |
|----------------|-------------------------|
| 1              | 4.4                     |
| 2              | 14.7                    |
| 3              | 29.5                    |
| 4              | 70.5                    |
| 5              | 85.3                    |
| 6              | 95.6                    |

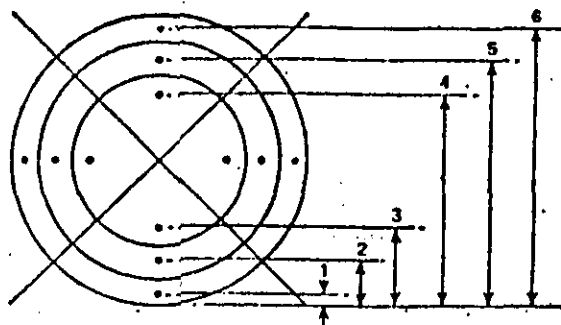


Figure 1-3. Example showing circular stack cross section divided into 12 equal areas, with location of traverse points indicated.

Table 1-2. LOCATION OF TRAVERSE POINTS IN CIRCULAR STACKS  
(Percent of stack diameter from inside wall to traverse point)

| Traverse point number on a diameter | Number of traverse points on a diameter |      |      |      |      |      |      |      |      |      |      |      |
|-------------------------------------|-----------------------------------------|------|------|------|------|------|------|------|------|------|------|------|
|                                     | 2                                       | 4    | 6    | 8    | 10   | 12   | 14   | 16   | 18   | 20   | 22   | 24   |
| 1                                   | 14.6                                    | 6.7  | 4.4  | 3.2  | 2.6  | 2.1  | 1.8  | 1.6  | 1.4  | 1.3  | 1.1  | 1.1  |
| 2                                   | 85.4                                    | 25.0 | 14.6 | 10.5 | 8.2  | 6.7  | 5.7  | 4.9  | 4.4  | 3.9  | 3.5  | 3.2  |
| 3                                   |                                         | 75.0 | 29.6 | 19.4 | 14.6 | 11.8 | 9.9  | 8.5  | 7.5  | 6.7  | 6.0  | 5.5  |
| 4                                   |                                         | 93.3 | 70.4 | 32.3 | 22.6 | 17.7 | 14.6 | 12.5 | 10.9 | 9.7  | 8.7  | 7.9  |
| 5                                   |                                         |      | 85.4 | 67.7 | 34.2 | 25.0 | 20.1 | 16.9 | 14.6 | 12.9 | 11.6 | 10.5 |
| 6                                   |                                         |      | 95.6 | 80.6 | 65.8 | 35.6 | 26.9 | 22.0 | 18.8 | 16.5 | 14.6 | 13.2 |
| 7                                   |                                         |      |      | 89.5 | 77.4 | 64.4 | 36.6 | 28.3 | 23.6 | 20.4 | 18.0 | 16.1 |
| 8                                   |                                         |      |      | 96.8 | 85.4 | 75.0 | 63.4 | 37.5 | 29.6 | 25.0 | 21.8 | 19.4 |
| 9                                   |                                         |      |      |      | 91.8 | 82.3 | 73.1 | 62.5 | 38.2 | 30.6 | 26.2 | 23.0 |
| 10                                  |                                         |      |      |      | 97.4 | 88.2 | 79.9 | 71.7 | 61.8 | 38.8 | 31.5 | 27.2 |
| 11                                  |                                         |      |      |      |      | 93.3 | 85.4 | 78.0 | 70.4 | 61.2 | 39.3 | 32.3 |
| 12                                  |                                         |      |      |      |      | 97.9 | 90.1 | 83.1 | 76.4 | 69.4 | 60.7 | 39.8 |
| 13                                  |                                         |      |      |      |      |      | 94.3 | 87.5 | 81.2 | 75.0 | 68.5 | 60.2 |
| 14                                  |                                         |      |      |      |      |      | 98.2 | 91.5 | 85.4 | 79.6 | 73.8 | 67.7 |
| 15                                  |                                         |      |      |      |      |      |      | 95.1 | 89.1 | 83.5 | 78.2 | 72.8 |
| 16                                  |                                         |      |      |      |      |      |      | 98.4 | 92.5 | 87.1 | 82.0 | 77.0 |
| 17                                  |                                         |      |      |      |      |      |      |      | 95.6 | 90.3 | 85.4 | 80.6 |
| 18                                  |                                         |      |      |      |      |      |      |      | 98.6 | 93.3 | 88.4 | 83.9 |
| 19                                  |                                         |      |      |      |      |      |      |      |      | 96.1 | 91.3 | 86.8 |
| 20                                  |                                         |      |      |      |      |      |      |      |      | 98.7 | 94.0 | 89.5 |
| 21                                  |                                         |      |      |      |      |      |      |      |      |      | 96.5 | 92.1 |
| 22                                  |                                         |      |      |      |      |      |      |      |      |      | 98.9 | 94.5 |
| 23                                  |                                         |      |      |      |      |      |      |      |      |      |      | 96.8 |
| 24                                  |                                         |      |      |      |      |      |      |      |      |      |      | 98.9 |

2.3.1.2 Stacks With Diameters Equal to or Less Than 0.61 m (24 in.). Follow the procedure in Section 2.3.1.1, noting only that any "adjusted" points should be relocated away from the stack walls to: (1) a distance of 1.3 cm (0.50 in.); or (2) a distance equal to the nozzle inside diameter, whichever is larger.

2.3.2 Rectangular Stacks. Determine the number of traverse points as explained in Sections 2.1 and 2.2 of this method. From Table 1-1, determine the grid configuration. Divide the stack cross-section into as many equal rectangular elemental areas as traverse points,

and then locate a traverse point at the centroid of each equal area according to the example in Figure 1-4.

The situation of traverse points being too close to the stack walls is not expected to arise with rectangular stacks. If this problem should ever arise, the Administrator must be contacted for resolution of the matter.

2.4 Verification of Absence of Cyclonic Flow. In most stationary sources, the direction of stack gas flow is essentially parallel to the stack walls. However, cyclonic flow may exist (1) after such devices as cyclones and inertial demisters following venturi scrubbers, or

(2) in stacks having tangential inlets or other duct configurations which tend to induce swirling; in these instances, the presence or absence of cyclonic flow at the sampling location must be determined. The following techniques are acceptable for this determination.

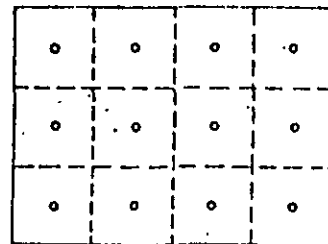


Figure 1-4. Example showing rectangular stack cross section divided into 12 equal areas, with a traverse point at centroid of each area.

Level and zero the manometer. Connect a Type B pitot tube to the manometer. Position the Type B pitot tube at each traverse point, in succession, so that the planes of the face openings of the pitot tube are perpendicular to the stack cross-sectional plane; when the Type B pitot tube is in this position, it is at "0" reference. Note the differential pressure ( $\Delta p$ ) reading at each traverse point. If a null (zero) pitot reading is obtained at 0° reference at a given traverse point, an acceptable flow condition exists at that point. If the pitot reading is not zero at 0° reference, rotate the pitot tube (up to  $\pm 90^\circ$  yaw angle), until a null reading is obtained. Carefully determine and record the value of the rotation angle ( $\alpha$ ) to the nearest degree. After the null technique has been applied at each traverse point, calculate the average of the absolute values of  $\alpha$ ; assign  $\alpha$  values of 0° to those points for which no rotation was required, and include those in the overall average. If the average value of  $\alpha$  is greater than 10°, the overall flow condition in the stack is unacceptable and alternative methodology, subject to the approval of the Administrator, must be used to perform accurate sample and velocity traverses.

### 3. Bibliography

1. Determining Dust Concentration in a Gas Stream. ASME Performance Test Code No. 27. New York, 1957.
2. Deworkin, Howard, et al. Air Pollution Source Testing Manual. Air Pollution Control District, Los Angeles, CA, November 1963.
3. Methods for Determination of Velocity, Volume, Dust and Mist Content of Gases. Western Precipitation Division of Joy Manufacturing Co. Los Angeles, CA. Bulletin WP-50, 1968.
4. Standard Method for Sampling Stacks for Particulate Matter. In: 1971 Book of ASTM Standards, Part 23. ASTM Designation D-2925-71. Philadelphia, Pa. 1971.
5. Hanson, H. A., et al. Particulate Sampling Strategies for Large Power Plants Including Nonuniform Flow. USEPA, ORD, ES-11, Research Triangle Park, N.C. EPA-600/2-76-170, June 1976.
6. Entropy Environmentalists, Inc. Determination of the Optimum Number of Sampling Points: An Analysis of Method 1 Criteria. Environmental Protection Agency, Research Triangle Park, N.C. EPA Contract No. 68-01-3172, Task 7.

### METHOD 2—DETERMINATION OF STACK GAS VELOCITY AND VOLUMETRIC FLOW RATE (TYPE B PITOT TUBE)

#### 1. Principle and Applicability

1.1 Principle. The average gas velocity in a stack is determined from the gas density and from measurement of the average velocity head with a Type S (Stauscheibe or reverse type) pitot tube.

1.2 Applicability. This method is applicable for measurement of the average velocity of a gas stream and for quantifying gas flow.

This procedure is not applicable at measurement sites which fail to meet the criteria of Method 1, Section 2.1. Also, the method cannot be used for direct measurement in cyclonic or swirling gas streams; Section 2.4 of Method 1 shows how to determine cyclonic or swirling flow conditions. When unacceptable conditions exist, alternative procedures, subject to the approval of the Administrator, U.S. Environmental Protection Agency, must be employed to make accurate flow rate determinations; examples of such alternative procedures are: (1) to install straightening vanes; (2) to calculate the total volumetric flow rate stoichiometrically, or (3) to move to another measurement site at which the flow is acceptable.

#### 2. Apparatus

Specifications for the apparatus are given below. Any other apparatus that has been demonstrated (subject to approval of the Administrator) to be capable of meeting the specifications will be considered acceptable.

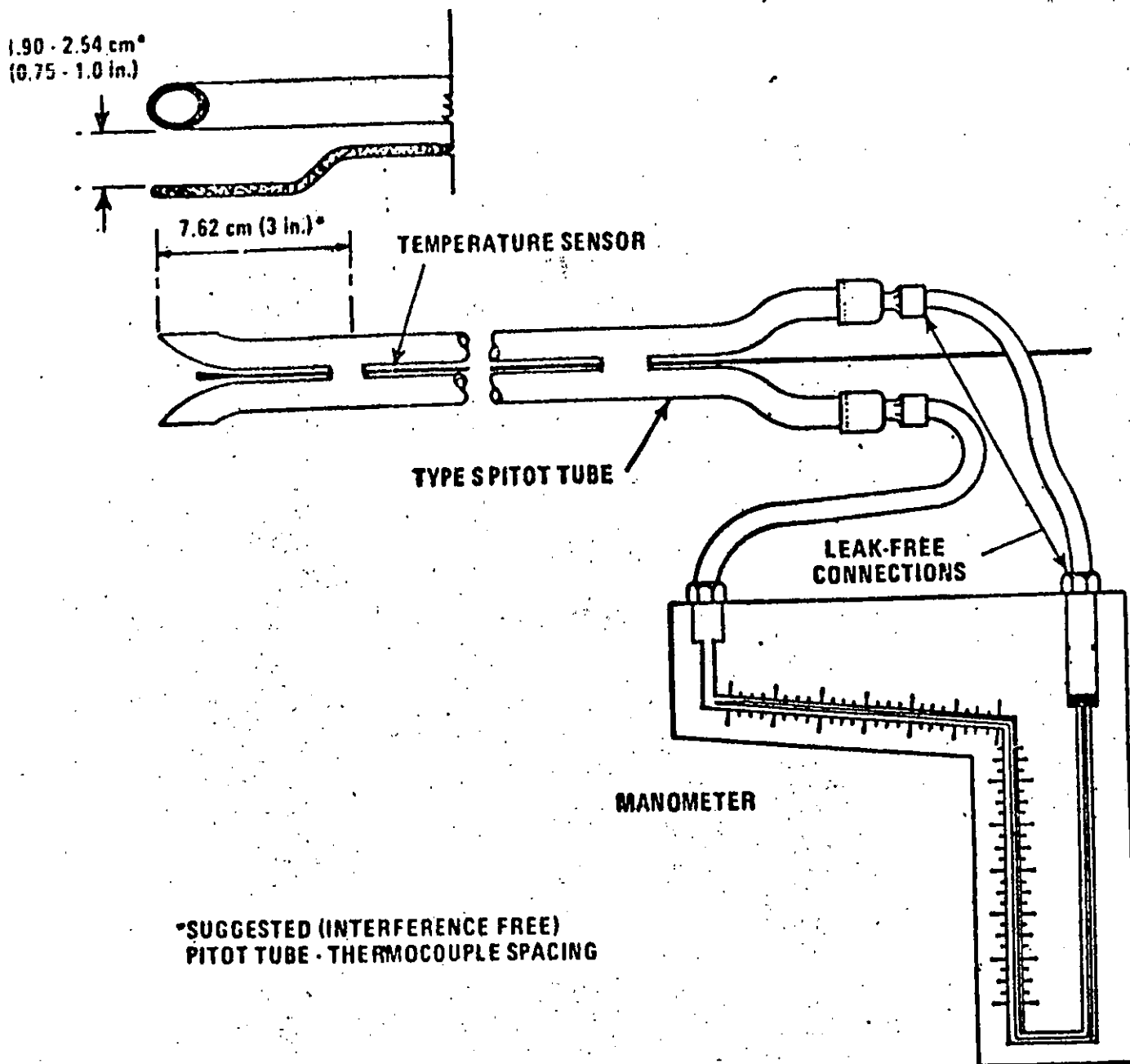


Figure 2-1. Type S pitot tube manometer assembly.

2.1 Type S Pitot Tube. The Type S pitot tube (Figure 2-1) shall be made of metal tubing (e.g., stainless steel). It is recommended that the external tubing diameter (dimension  $D_1$ , Figure 2-2b) be between 0.48 and 0.95 centimeters (3/16 and 1/4 inch). There shall be an equal distance from the base of each leg of the pitot tube to its face-opening plane (dimensions  $P_1$  and  $P_2$ , Figure 2-2b); it is recommended that this distance be between 1.03 and 1.50 times the external tubing diameter. The face openings of the pitot tube shall, preferably, be aligned as shown in Figure 2-2; however, slight misalignments of the openings are permissible (see Figure 2-3). The Type S pitot tube shall have a known coefficient, determined as outlined in Section 4. An identification number shall be assigned to the pitot tube; this number shall be permanently marked or engraved on the body of the tube.

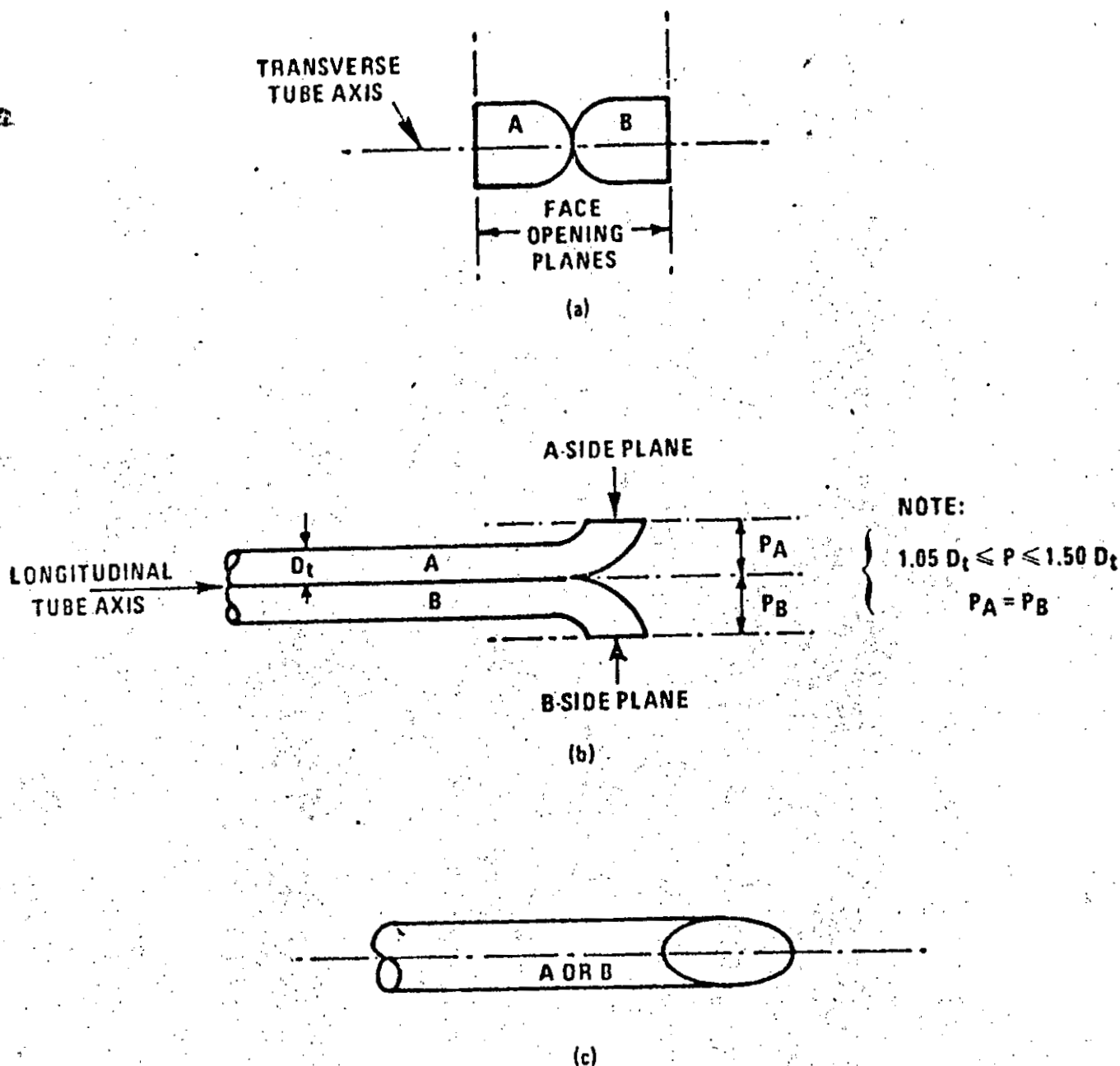


Figure 2-2. Properly constructed Type S pitot tube, shown in: (a) end view; face opening planes perpendicular to transverse axis; (b) top view; face opening planes parallel to longitudinal axis; (c) side view; both legs of equal length and centerlines coincident, when viewed from both sides. Base-line coefficient values of 0.84 may be assigned to pitot tubes constructed this way.

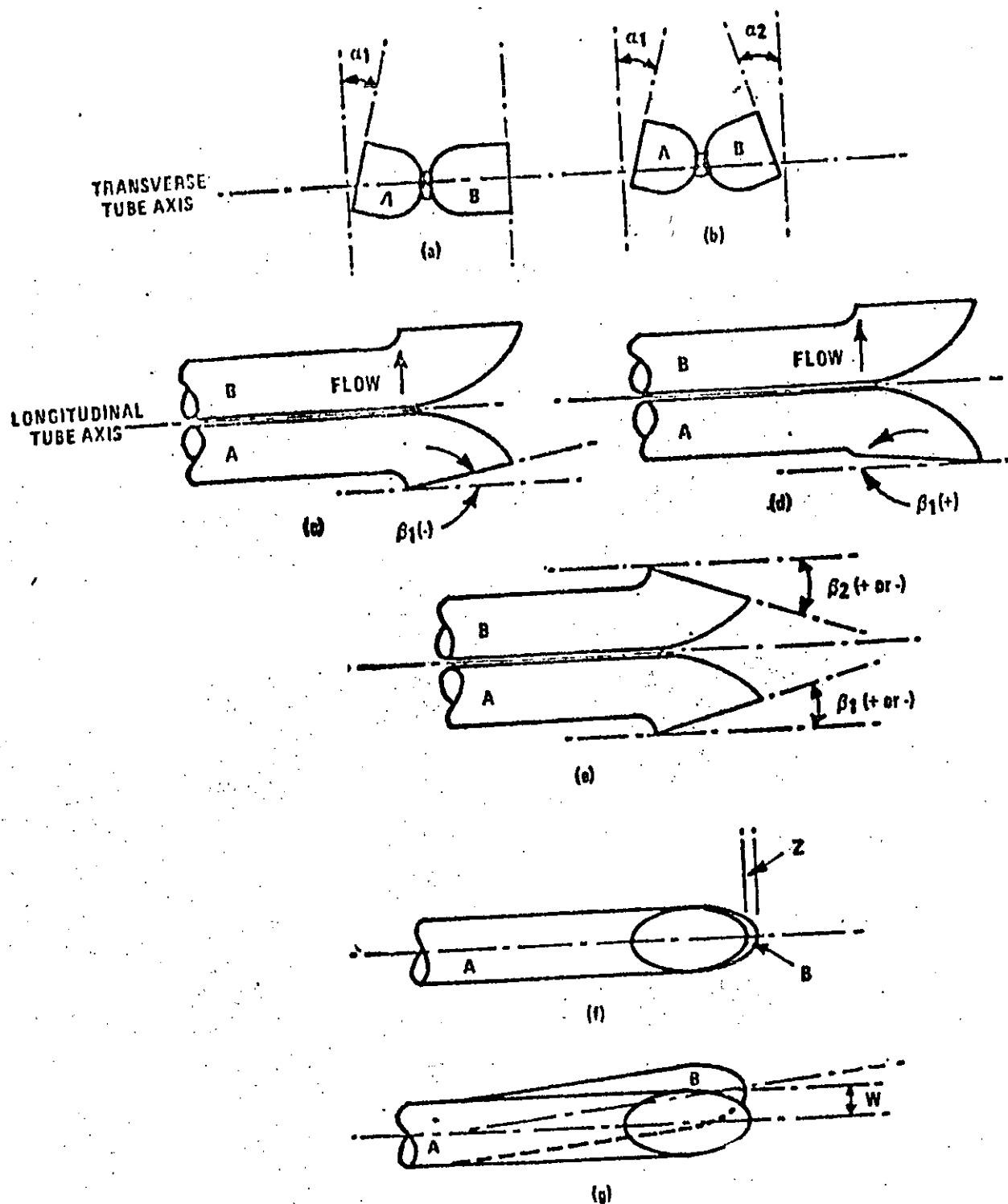


Figure 2-3. Types of face-opening misalignment that can result from field use or improper construction of Type S pitot tubes. These will not affect the baseline value of  $\bar{C}_p(s)$  so long as  $\alpha_1$  and  $\alpha_2 < 10^\circ$ ,  $\beta_1$  and  $\beta_2 < 5^\circ$ ,  $z < 0.32$  cm (1/8 in.) and  $w < 0.08$  cm (1/32 in.) (citation 11 in Section 6).



[illegible]

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10. Determine the stack gas dry molecular weight. For combustion processes at pressures that exist essentially at 101.3 kPa (14.7 psia) and  $N_2$ , use Method 3. For processes at pressures essentially at 101.3 kPa (14.7 psia) and  $N_2$ , use Method 4. For other processes, use a dry molecular weight of 29.0. For other processes, other methods, subject to the approval of the Administrator, must be used.

11. Obtain the moisture content from Reference Method 3 (or equivalent) or from Method 6.

12. Determine the cross-sectional area of the stack or duct at the sampling location. Whenever possible, physically measure the stack dimensions rather than using blueprints.

#### 4. Calibration

4.1. Type 8 Pitot Tube. Before its initial use, carefully examine the Type 8 pitot tube in top, side, and end views to verify that the face openings of the tube are aligned within the specifications illustrated in Figure 2-6 or 2-7. The pitot tube shall not be used if it fails to meet these alignment specifications.

After verifying the face opening alignment, measure and record the following dimensions of the pitot tube:

(a) the external tubing diameter (denoted  $D_t$ , Figure 2-2b); and (b) the base-to-impact plane distance (denoted  $P_2$  and  $P_3$ , Figure 2-2b). If  $D_t$  is between 0.48 and 0.95 cm (1/4 and 3/8 in.) and  $P_2$  and  $P_3$  are equal and between 1.93 and 1.97 cm (3/4 and 3/8 in.), the pitot tube may be calibrated according to the procedure outlined in Sections 4.1.2 through 4.1.5 below, or (2) a baseline isolated probe coefficient value of 0.81 may be used for the pitot tube. Note, however, that if the pitot tube is part of an assembly, calibration may still be required, despite knowledge of the baseline coefficient value (see Section 4.1.1).

If  $D_t$ ,  $P_2$ , and  $P_3$  are outside the specified limits, the pitot tube must be calibrated as outlined in 4.1.2 through 4.1.5 below.

4.1.1. Type 8 Pitot Tube Assemblies. During sample and velocity traverses, the isolated Type 8 pitot tube is not always used; in many instances, the pitot tube is used in combination with other sense-sampling components (thermocouple, sampling probe, nozzle) as part of an "assembly." The presence of other sampling components can sometimes affect the baseline value of the Type 8 pitot tube coefficient (Citation 9 in Section 6); therefore an assigned (or otherwise known) baseline coefficient

value may or may not be valid for a given assembly. The baseline and assembly coefficient values will be identical only when the relative placement of the components in the assembly is such that aerodynamic interference effects are eliminated. Figures 2-6 through 2-8 illustrate interference-free measurement arrangements for Type 8 pitot tubes having external tubing diameters between 0.48 and 0.95 cm (1/4 and 3/8 in.). Type 8 pitot tube assemblies that fail to meet any or all of the specifications of Figures 2-6 through 2-8 shall be calibrated according to the procedure outlined in Sections 4.1.2 through 4.1.5 below, and prior to calibration, the values of the inter-component spacing (pitot-nozzle, pitot-thermocouple, pitot-probe sheath) shall be measured and recorded.

Note.—Do not use any Type 8 pitot tube assembly which is constructed such that the impact pressure opening plane of the pitot tube is below the entry plane of the nozzle (see Figure 2-6b).

4.1.2. Calibration Setup. If the Type 8 pitot tube is to be calibrated, one leg of the tube shall be permanently marked A, and the other, 1. Calibration shall be done in a flow system having the following essential design features:

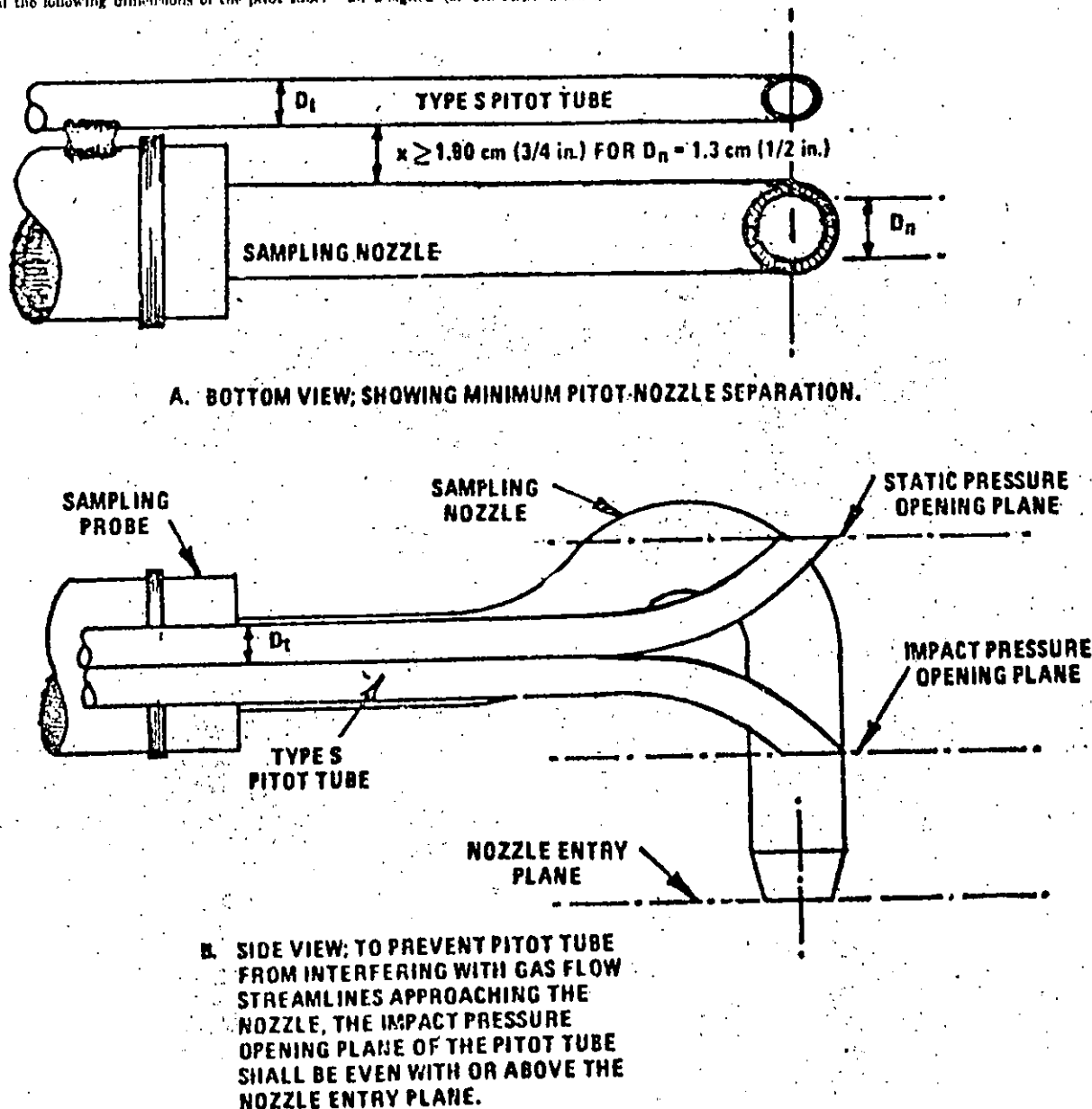


Figure 2-6. Proper pitot tube - sampling nozzle configuration to prevent aerodynamic interference; buttonhook - type nozzle; centers of nozzle and pitot opening aligned;  $D_t$  between 0.48 and 0.95 cm (3/16 and 3/8 in.).



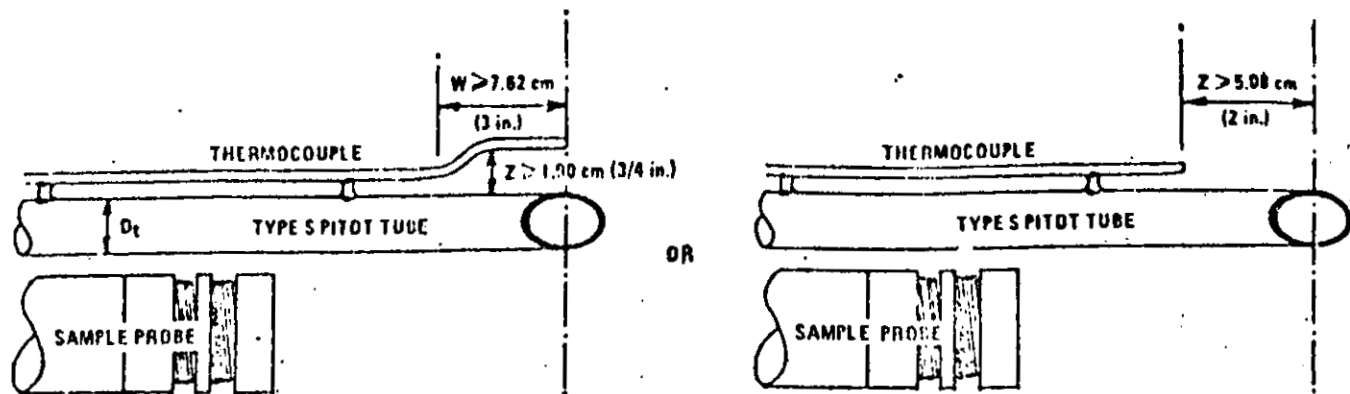


Figure 2-7. Proper thermocouple placement to prevent interference;  $D_t$  between 0.48 and 0.95 cm (3/16 and 3/8 in.).

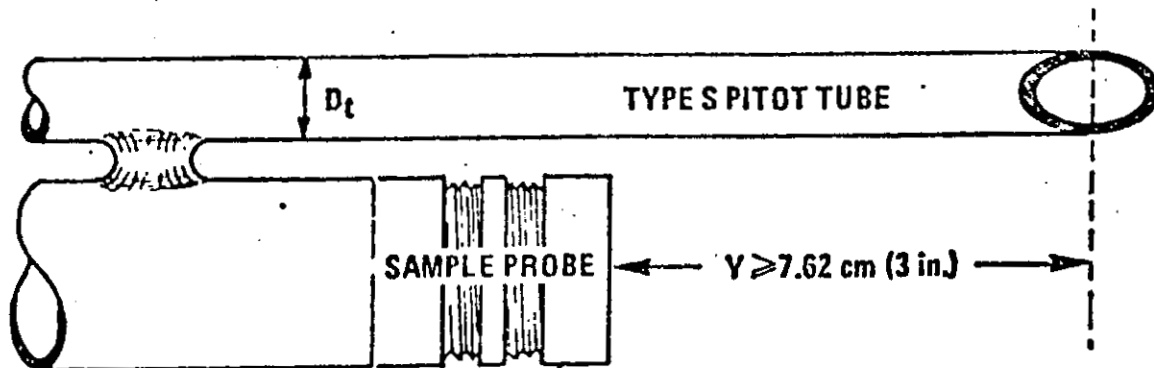


Figure 2-8. Minimum pitot-sample probe separation needed to prevent interference;  $D_t$  between 0.48 and 0.95 cm (3/16 and 3/8 in.).

4.1.2.1 The flowing gas stream must be confined to a duct of definite cross-sectional area, either circular or rectangular. For circular cross-sections, the minimum duct diameter shall be 30.5 cm (12 in.); for rectangular cross-sections, the width (shorter side) shall be at least 25.4 cm (10 in.).

4.1.2.2 The cross-sectional area of the calibration duct must be constant over a distance of 10 or more duct diameters. For a rectangular cross-section, use an equivalent diameter, calculated from the following equation, to determine the number of duct diameters:

$$D_e = \frac{2LW}{L+W}$$

Equation 2-1

where:

$D_e$  = Equivalent diameter  
 $L$  = Length  
 $W$  = Width

To ensure the presence of stable, fully developed flow patterns at the calibration site, or "test section," the site must be located at least eight diameters downstream and two diameters upstream from the nearest disturbances.

Note.—The eight- and two-diameter criteria are not absolute; other test section locations may be used (subject to approval of the Administrator), provided that the flow at the test site is stable and demonstrably parallel to the duct axis.

4.1.2.3 The flow system shall have the capacity to generate a test-section velocity around 915 m/min (3,000

ft/min). This velocity must be constant with time to guarantee steady flow during calibration. Note that Type S pitot tube coefficients obtained by single-velocity calibration at 915 m/min (3,000 ft/min) will generally be valid to within  $\pm 3$  percent for the measurement of velocities above 305 m/min (1,000 ft/min) and to within  $\pm 5$  to 6 percent for the measurement of velocities between 180 and 305 m/min (600 and 1,000 ft/min). If a more precise correlation between  $C_p$  and velocity is desired, the flow system shall have the capacity to generate at least four distinct, time-invariant test-section velocities covering the velocity range from 180 to 1,825 m/min (600 to 5,990 ft/min), and calibration data shall be taken at regular velocity intervals over this range (see Citations 9 and 14 in Section 6 for details).

4.1.2.4 Two entry ports, one each for the standard and Type S pitot tubes, shall be cut in the test section; the standard pitot entry port shall be located slightly downstream of the Type S port, so that the standard and Type S impact openings will lie in the same cross-sectional plane during calibration. To facilitate alignment of the pitot tubes during calibration, it is advisable that the test section be constructed of plexiglas or some other transparent material.

4.1.3 Calibration Procedure. Note that this procedure is a general one and must not be used without first referring to the special considerations presented in Section 4.1.5. Note also that this procedure applies only to single-velocity calibration. To obtain calibration data for the A and B sides of the Type S pitot tube, proceed as follows:

4.1.3.1 Make sure that the manometer is properly filled and that the oil is free from contamination and that of the proper density. Inspect and leak check all pitot lines; repair or replace if necessary.

4.1.3.2 Level and zero the manometer. Turn on the fan and allow the flow to stabilize. Seal the Type S entry port.

4.1.3.3 Ensure that the manometer is level and zeroed. Position the standard pitot tube at the calibration point (determined as outlined in Section 4.1.5.1), and align the tube so that its tip is pointed directly into the flow. Particular care should be taken in aligning the tube to avoid yaw and pitch angles. Make sure that the entry port surrounding the tube is properly sealed.

4.1.3.4 Read  $\Delta P_{std}$  and record its value in a data table similar to the one shown in Figure 2-9. Remove the standard pitot tube from the duct and disconnect it from the manometer. Seal the standard entry port.

4.1.3.5 Connect the Type S pitot tube to the manometer. Open the Type S entry port. Check the manometer level and zero. Insert and align the Type S pitot tube so that its A side impact opening is at the same point as was the standard pitot tube and is pointed directly into the flow. Make sure that the entry port surrounding the tube is properly sealed.

4.1.3.6 Read  $\Delta P_s$  and enter its value in the data table. Remove the Type S pitot tube from the duct and disconnect it from the manometer.

4.1.3.7 Repeat steps 4.1.3.3 through 4.1.3.6 above until three pairs of  $\Delta P$  readings have been obtained.

4.1.3.8 Repeat steps 4.1.3.3 through 4.1.3.7 above for the B side of the Type S pitot tube.

4.1.3.9 Perform calculations, as described in Section 4.1.4 below.

4.1.4 Calculations.

4.1.4.1 For each of the six pairs of  $\Delta P$  readings (i.e., three from side A and three from side B) obtained in Section 4.1.3 above, calculate the value of the Type S pitot tube coefficient as follows:

PITOT TUBE IDENTIFICATION NUMBER: \_\_\_\_\_ DATE: \_\_\_\_\_  
 CALIBRATED BY: \_\_\_\_\_

| "A" SIDE CALIBRATION |                                                                   |                                                                |                      |                                      |
|----------------------|-------------------------------------------------------------------|----------------------------------------------------------------|----------------------|--------------------------------------|
| RUN NO.              | $\Delta p_{std}$<br>cm H <sub>2</sub> O<br>(in. H <sub>2</sub> O) | $\Delta p(s)$<br>cm H <sub>2</sub> O<br>(in. H <sub>2</sub> O) | $C_p(s)$             | DEVIATION<br>$C_p(s) - \bar{C}_p(A)$ |
| 1                    |                                                                   |                                                                |                      |                                      |
| 2                    |                                                                   |                                                                |                      |                                      |
| 3                    |                                                                   |                                                                |                      |                                      |
|                      |                                                                   |                                                                | $\bar{C}_p$ (SIDE A) |                                      |

| "B" SIDE CALIBRATION |                                                                   |                                                                |                      |                                      |
|----------------------|-------------------------------------------------------------------|----------------------------------------------------------------|----------------------|--------------------------------------|
| RUN NO.              | $\Delta p_{std}$<br>cm H <sub>2</sub> O<br>(in. H <sub>2</sub> O) | $\Delta p(s)$<br>cm H <sub>2</sub> O<br>(in. H <sub>2</sub> O) | $C_p(s)$             | DEVIATION<br>$C_p(s) - \bar{C}_p(B)$ |
| 1                    |                                                                   |                                                                |                      |                                      |
| 2                    |                                                                   |                                                                |                      |                                      |
| 3                    |                                                                   |                                                                |                      |                                      |
|                      |                                                                   |                                                                | $\bar{C}_p$ (SIDE B) |                                      |

$$\text{AVERAGE DEVIATION} = \sigma(A \text{ OR } B) = \frac{\sum_{i=1}^3 |C_p(s) - \bar{C}_p(A \text{ OR } B)|}{3} \leftarrow \text{MUST BE } < 0.01$$

$$|\bar{C}_p(\text{SIDE A}) - \bar{C}_p(\text{SIDE B})| \leftarrow \text{MUST BE } < 0.01$$

Figure 2-9. Pitot tube calibration data.

$$C_{p(s)} = C_{p(std)} \sqrt{\frac{\Delta p_{std}}{\Delta p_s}}$$

Equation 2-2

where:

$C_{p(s)}$  = Type B pitot tube coefficient  
 $C_{p(std)}$  = Standard pitot tube coefficient; use 0.99 if the coefficient is unknown and the tube is designed

according to the criteria of Sections 2.7.1 to 2.7.6 of this method.  
 $\Delta p_{std}$  = Velocity head measured by the standard pitot tube, cm H<sub>2</sub>O (in. H<sub>2</sub>O)  
 $\Delta p_s$  = Velocity head measured by the Type B pitot tube, cm H<sub>2</sub>O (in. H<sub>2</sub>O)

4.1.4.3 Calculate  $\bar{C}_p$  (side A), the mean A-side coefficient, and  $\bar{C}_p$  (side B), the mean B-side coefficient; calculate the difference between these two average values.

4.1.4.3 Calculate the deviation of each of the three A side values of  $C_{p(s)}$  from  $\bar{C}_p$  (side A), and the deviation of each B side value of  $C_{p(s)}$  from  $\bar{C}_p$  (side B). Use the following equation:

$$\text{Deviation} = C_{p(s)} - \bar{C}_p(A \text{ or } B)$$

Equation 2-3

4.1.4.4 Calculate  $\sigma$ , the average deviation from the mean, for both the A and B sides of the pitot tube. Use the following equation:

$$\sigma(\text{side A or B}) = \frac{\sum_{i=1}^3 |C_{p(s)} - \bar{C}_p(A \text{ or } B)|}{3}$$

Equation 2-4

4.1.4.5 Use the Type B pitot tube only if the values of  $\sigma$  (side A) and  $\sigma$  (side B) are less than or equal to 0.01 and if the absolute value of the difference between  $\bar{C}_p$  (A) and  $\bar{C}_p$  (B) is 0.01 or less.

4.1.5 Special considerations.

4.1.5.1 Selection of calibration point.

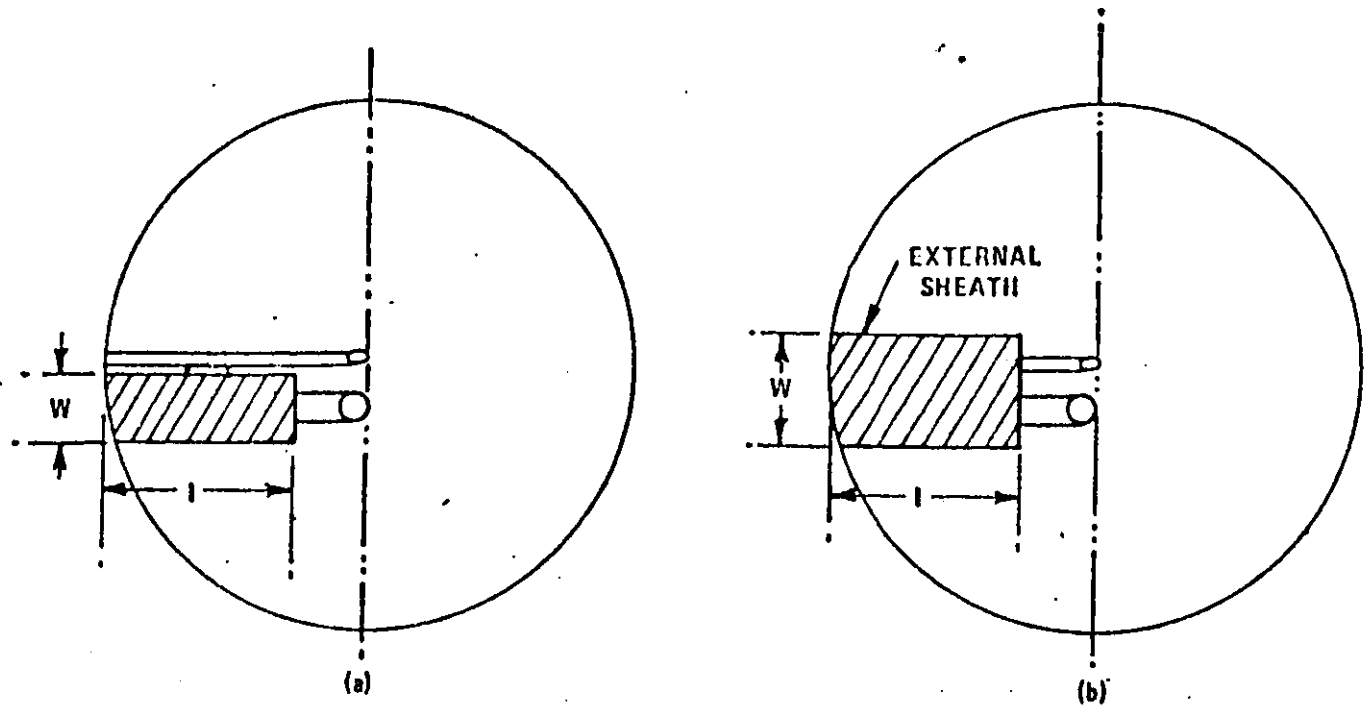
4.1.5.1.1 When an isolated Type B pitot tube is calibrated, select a calibration point at or near the center of the duct, and follow the procedures outlined in Sections 4.1.3 and 4.1.4 above. The Type B pitot coefficients so obtained, i.e.,  $\bar{C}_p$  (side A) and  $\bar{C}_p$  (side B), will be valid, so long as either: (1) the isolated pitot tube is used; or (2) the pitot tube is used with other components (nozzle, thermocouple, sample probe) in an arrangement that is free from aerodynamic interference effects (see Figures 2-6 through 2-8).

4.1.5.1.2 For Type B pitot tube-thermocouple combinations (without sample probe), select a calibration point at or near the center of the duct, and follow the procedures outlined in Sections 4.1.3 and 4.1.4 above. The coefficients so obtained will be valid so long as the pitot tube-thermocouple combination is used by itself or with other components in an interference-free arrangement (Figures 2-6 and 2-8).

4.1.5.1.3 For assemblies with sample probes, the calibration point should be located at or near the center of the duct; however, insertion of a probe sheath into a small duct may cause significant cross-sectional area blockage and yield incorrect coefficient values (Citation 9 in Section 6). Therefore, to minimize the blockage effect, the calibration point may be a few inches off-center if necessary. The actual blockage effect will be negligible when the theoretical blockage, as determined by a projected-area model of the probe sheath, is 2 percent or less of the duct cross-sectional area for assemblies without external sheaths (Figure 2-10a), and 3 percent or less for assemblies with external sheaths (Figure 2-10b).

4.1.5.2 For those probe assemblies in which pitot tube-nozzle interference is a factor (i.e., those in which the pitot-nozzle separation distance fails to meet the specification illustrated in Figure 2-6a), the value of  $C_{p(s)}$  depends upon the amount of free space between the tube and nozzle, and therefore is a function of nozzle size. In these instances, separate calibrations shall be performed with each of the commonly used nozzle sizes in place. Note that the single-velocity calibration technique is acceptable for this purpose, even though the larger nozzle sizes (>0.635 cm or 1/4 in.) are not ordinarily used for isokinetic sampling at velocities around 915 m/min (3,000 ft/min), which is the calibration velocity; note also that it is not necessary to draw an isokinetic sample during calibration (see Citation 19 in Section 6).

4.1.5.3 For a probe assembly constructed such that its pitot tube is always used in the same orientation, only one side of the pitot tube need be calibrated (the side which will face the flow). The pitot tube must still meet the alignment specifications of Figure 2-2 or 2-3, however, and must have an average deviation ( $\sigma$ ) value of 0.01 or less (see Section 4.1.4.4).



$$\text{ESTIMATED SHEATH BLOCKAGE (\%)} = \left[ \frac{1 \times W}{\text{DUCT AREA}} \right] \times 100$$

Figure 2-10. Projected-area models for typical pitot tube assemblies.

#### 4.1.6 Field Use and Recalibration.

4.1.6.1 Field Use. When a Type S pitot tube (isolated tube or assembly) is used in the field, the appropriate coefficient value (whether assigned or obtained by calibration) shall be used to perform velocity calculations. For calibrated Type S pitot tubes, the A side coefficient shall be used when the A side of the tube faces the flow, and the B side coefficient shall be used when the B side faces the flow; alternatively, the arithmetic average of the A and B side coefficient values may be used, irrespective of which side faces the flow.

4.1.6.1.2 When a probe assembly is used to sample a small duct (12 to 36 in. in diameter), the probe should sometimes block a significant part of the duct cross-section, causing a reduction in the effective value of  $T_{st}$ . Consult Citation 6 in Section 6 for details. Conventional point-sampling probe assemblies are not recommended for use in ducts having inside diameters smaller than 12 inches (Citation 16 in Section 6).

#### 4.1.6.2 Recalibration.

4.1.6.2.1 Isolated Pitot Tubes. After each field use, the pitot tube shall be carefully reexamined in top, side, and end views. If the pitot face openings are still aligned within the specifications illustrated in Figure 2-2 or 2-3, it can be assumed that the baseline coefficient of the pitot tube has not changed. If, however, the tube has been damaged to the extent that it no longer meets the specifications of Figure 2-2 or 2-3, the damage shall either be repaired to restore proper alignment of the face openings or the tube shall be discarded.

4.1.6.2.2 Pitot Tube Assemblies. After each field use, check the face opening alignment of the pitot tube, as in Section 4.1.6.2.1; also, reexamine the intercomponent spacings of the assembly. If the intercomponent spacings have not changed and the face opening alignment is acceptable, it can be assumed that the coefficient of the assembly has not changed. If the face opening alignment is no longer within the specifications of Figures 2-2 or 2-3, either repair the damage or replace the pitot tube (calibrating the new assembly, if necessary). If the intercomponent spacings have changed, restore the original spacings or recalibrate the assembly.

4.2 Standard pitot tube (if applicable). If a standard pitot tube is used for the velocity traverse, the tube shall be constructed according to the criteria of Section 2.7 and shall be assigned a baseline coefficient value of 0.99. If the standard pitot tube is used as part of an assembly,

the tube shall be in an interference-free arrangement (subject to the approval of the Administrator).

4.3 Temperature Gauges. After each field use, calibrate dial thermometers, liquid-filled bulb thermometers, thermocouple-potentiometer systems, and other gauges at a temperature within 10 percent of the average absolute stack temperature. For temperatures up to 405° C (761° F), use an ASTM mercury-in-glass reference thermometer, or equivalent, as a reference; alternatively, either a reference thermocouple and potentiometer (calibrated by NIST) or thermometric fixed points, e.g., ice bath and boiling water (corrected for barometric pressure) may be used. For temperatures above 405° C (761° F), use an NBS-calibrated reference thermocouple-potentiometer system or an alternate reference, subject to the approval of the Administrator.

If, during calibration, the absolute temperatures measured with the gauge being calibrated and the reference gauge agree within 1.5 percent, the temperature data taken in the field shall be considered valid. Otherwise, the pollutant emission test shall either be considered invalid or adjustments (if appropriate) of the test results shall be made, subject to the approval of the Administrator.

4.4 Barometer. Calibrate the barometer used against a mercury barometer.

#### 5. Calculations

Carry out calculations, retaining at least one extra decimal figure beyond that of the acquired data. Round off figures after final calculation.

##### 5.1 Nomenclature.

$A$  = Cross-sectional area of stack,  $m^2$  ( $ft^2$ ).  
 $B_w$  = Water vapor in the gas stream (from Method 5 or Reference Method 4), proportion by volume.  
 $C_p$  = Pitot tube coefficient, dimensionless.  
 $K_p$  = Pitot tube constant.

$$34.07 \frac{m}{sec} \left[ \frac{(\rho \text{ g-mole}) (mm Hg)}{(^{\circ}K) (mm H_2O)} \right]^{1/2}$$

for the metric system and

$$85.40 \frac{ft}{sec} \left[ \frac{(\text{lb/lb-mole}) (in. Hg)}{(^{\circ}F) (in. H_2O)} \right]^{1/2}$$

for the English system.

$M_d$  = Molecular weight of stack gas, dry basis (see Section 3.6) g/g-mole (lb/lb-mole).  
 $M_w$  = Molecular weight of stack gas, wet basis, g/g-mole (lb/lb-mole).

$$= M_d (1 - B_w) + 18.0 B_w \quad \text{Equation 2-3}$$

$P_{bar}$  = Barometric pressure at measurement site, mm Hg (in. Hg).

$P_s$  = Stack static pressure, mm Hg (in. Hg).

$P_a$  = Absolute stack gas pressure, mm Hg (in. Hg).

$$= P_{bar} + P_s \quad \text{Equation 2-4}$$

$P_{std}$  = Standard absolute pressure, 760 mm Hg (29.92 in. Hg).

$Q_{sd}$  = Dry volumetric stack gas flow rate corrected to standard conditions,  $dscm/hr$  ( $dscf/hr$ ).

$t_s$  = Stack temperature,  $^{\circ}C$  ( $^{\circ}F$ ).

$T_s$  = Absolute stack temperature,  $^{\circ}K$  ( $^{\circ}R$ ).

$$= 273 + t_s \text{ for metric} \quad \text{Equation 2-7}$$

$$= 460 + t_s \text{ for English} \quad \text{Equation 2-8}$$

$T_{std}$  = Standard absolute temperature, 273  $^{\circ}K$  (528  $^{\circ}R$ ).

$v_s$  = Average stack gas velocity,  $m/sec$  ( $ft/sec$ ).

$\Delta p$  = Velocity head of stack gas, mm H<sub>2</sub>O (in. H<sub>2</sub>O).

3,600 = Conversion factor,  $sec/hr$ .

18.0 = Molecular weight of water, g/g-mole (lb-lb-mole).

#### 5.2 Average stack gas velocity.

$$v_s = K_p C_p (\sqrt{\Delta p})_{avg} \sqrt{\frac{T_{std}}{P_s M_d}}$$

$$\text{Equation 2-9}$$

#### 5.3 Average stack gas dry volumetric flow rate.

$$Q_{sd} = 3,600 (1 - B_w) v_s A \left( \frac{T_{std}}{T_{s(avg)}} \right) \left( \frac{P_s}{P_{std}} \right)$$

$$\text{Equation 2-10}$$

#### 6. Bibliography

1. Mark, L. B. Mechanical Engineers' Handbook. New York, McGraw-Hill Book Co., Inc. 1951.
2. Perry, J. H. Chemical Engineers' Handbook. New York, McGraw-Hill Book Co., Inc. 1960.

## RULES AND REGULATIONS

PITOT TUBE IDENTIFICATION NUMBER: \_\_\_\_\_

DATE: \_\_\_\_\_

CALIBRATED BY: \_\_\_\_\_

| "A" SIDE CALIBRATION |                                                                   |                                                                |                      |                                      |
|----------------------|-------------------------------------------------------------------|----------------------------------------------------------------|----------------------|--------------------------------------|
| RUN NO.              | $\Delta p_{std}$<br>cm H <sub>2</sub> O<br>(in. H <sub>2</sub> O) | $\Delta p(s)$<br>cm H <sub>2</sub> O<br>(in. H <sub>2</sub> O) | $C_p(s)$             | DEVIATION<br>$C_p(s) - \bar{C}_p(A)$ |
| 1                    |                                                                   |                                                                |                      |                                      |
| 2                    |                                                                   |                                                                |                      |                                      |
| 3                    |                                                                   |                                                                |                      |                                      |
|                      |                                                                   |                                                                | $\bar{C}_p$ (SIDE A) |                                      |

| "B" SIDE CALIBRATION |                                                                   |                                                                |                      |                                      |
|----------------------|-------------------------------------------------------------------|----------------------------------------------------------------|----------------------|--------------------------------------|
| RUN NO.              | $\Delta p_{std}$<br>cm H <sub>2</sub> O<br>(in. H <sub>2</sub> O) | $\Delta p(s)$<br>cm H <sub>2</sub> O<br>(in. H <sub>2</sub> O) | $C_p(s)$             | DEVIATION<br>$C_p(s) - \bar{C}_p(B)$ |
| 1                    |                                                                   |                                                                |                      |                                      |
| 2                    |                                                                   |                                                                |                      |                                      |
| 3                    |                                                                   |                                                                |                      |                                      |
|                      |                                                                   |                                                                | $\bar{C}_p$ (SIDE B) |                                      |

$$\text{AVERAGE DEVIATION} = \sigma (A \text{ OR } B) = \frac{\sum_{i=1}^3 |C_p(s) - \bar{C}_p(A \text{ OR } B)|}{3} \leftarrow \text{MUST BE } < 0.01$$

$$|\bar{C}_p(\text{SIDE A}) - \bar{C}_p(\text{SIDE B})| \leftarrow \text{MUST BE } < 0.01$$

Figure 2-9. Pitot tube calibration data.

$$C_{p(s)} = C_{p(std)} \sqrt{\frac{\Delta p_{std}}{\Delta p_s}}$$

Equation 2-2

where:

 $C_{p(s)}$  = Type B pitot tube coefficient $C_{p(std)}$  = Standard pitot tube coefficient; use 0.99 if the coefficient is unknown and the tube is designed

according to the criteria of Sections 2.7.1 to 2.7.5 of this method.

 $\Delta p_{std}$  = Velocity head measured by the standard pitot tube, cm H<sub>2</sub>O (in. H<sub>2</sub>O) $\Delta p_s$  = Velocity head measured by the Type B pitot tube, cm H<sub>2</sub>O (in. H<sub>2</sub>O)4.1.4.2 Calculate  $\bar{C}_p$  (side A), the mean A-side coefficient, and  $\bar{C}_p$  (side B), the mean B-side coefficient; calculate the difference between these two average values.

4.1.4.3 Calculate the deviation of each of the three A-side values of  $C_{p(s)}$  from  $\bar{C}_p$  (side A), and the deviation of each B-side value of  $C_{p(s)}$  from  $\bar{C}_p$  (side B). Use the following equation:

$$\text{Deviation} = C_{p(s)} - \bar{C}_p(A \text{ or } B)$$

Equation 2-3

4.1.4.4 Calculate  $\sigma$ , the average deviation from the mean, for both the A and B sides of the pitot tube. Use the following equation:

$$\sigma (\text{side A or B}) = \frac{\sum_{i=1}^3 |C_{p(s)} - \bar{C}_p(A \text{ or } B)|}{3}$$

Equation 2-4

4.1.4.5 Use the Type B pitot tube only if the values of  $\sigma$  (side A) and  $\sigma$  (side B) are less than or equal to 0.01 and if the absolute value of the difference between  $\bar{C}_p$  (A) and  $\bar{C}_p$  (B) is 0.01 or less.

4.1.5 Special considerations.

4.1.5.1 Selection of calibration point.

4.1.5.1.1 When an isolated Type B pitot tube is calibrated, select a calibration point at or near the center of the duct, and follow the procedures outlined in Sections 4.1.3 and 4.1.4 above. The Type B pitot coefficients so obtained, i.e.,  $\bar{C}_p$  (side A) and  $\bar{C}_p$  (side B), will be valid, so long as either: (1) the isolated pitot tube is used; or (2) the pitot tube is used with other components (nozzle, thermocouple, sample probe) in an arrangement that is free from aerodynamic interference effects (see Figures 2-6 through 2-8).

4.1.5.1.2 For Type B pitot tube-thermocouple combinations (without sample probe), select a calibration point at or near the center of the duct, and follow the procedures outlined in Sections 4.1.3 and 4.1.4 above. The coefficients so obtained will be valid so long as the pitot tube-thermocouple combination is used by itself or with other components in an interference-free arrangement (Figures 2-6 and 2-8).

4.1.5.1.3 For assemblies with sample probes, the calibration point should be located at or near the center of the duct; however, insertion of a probe sheath into a small duct may cause significant cross-sectional area blockage and yield incorrect coefficient values (Citation 9 in Section 6). Therefore, to minimize the blockage effect, the calibration point may be a few inches off-center if necessary. The actual blockage effect will be negligible when the theoretical blockage, as determined by a projected-area model of the probe sheath, is 2 percent or less of the duct cross-sectional area for assemblies without external sheaths (Figure 2-10a), and 3 percent or less for assemblies with external sheaths (Figure 2-10b).

4.1.5.2 For those probe assemblies in which pitot tube-nozzle interference is a factor (i.e., those in which the pitot-nozzle separation distance fails to meet the specification illustrated in Figure 2-6a), the value of  $C_{p(s)}$  depends upon the amount of free space between the tube and nozzle, and therefore is a function of nozzle size. In these instances, separate calibrations shall be performed with each of the commonly used nozzle sizes in place. Note that the single-velocity calibration technique is acceptable for this purpose, even though the larger nozzle sizes ( $> 0.635$  cm or 1/4 in.) are not ordinarily used for isokinetic sampling at velocities around 915 ft/min (3.00 ft/min), which is the calibration velocity; note also that it is not necessary to draw an isokinetic sample during calibration (see Citation 12 in Section 6).

4.1.5.3 For a probe assembly constructed such that its pitot tube is always used in the same orientation, only one side of the pitot tube need be calibrated (the side which will face the flow). The pitot tube must still meet the alignment specifications of Figure 2-2 or 2-3, however, and must have an average deviation (a) value of 0.01 or less (see Section 4.1.4.4).

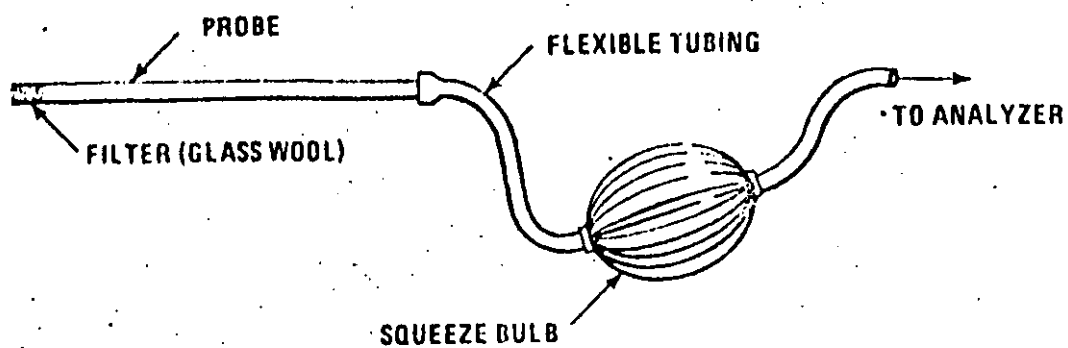


Figure 3-1. Grab-sampling train.

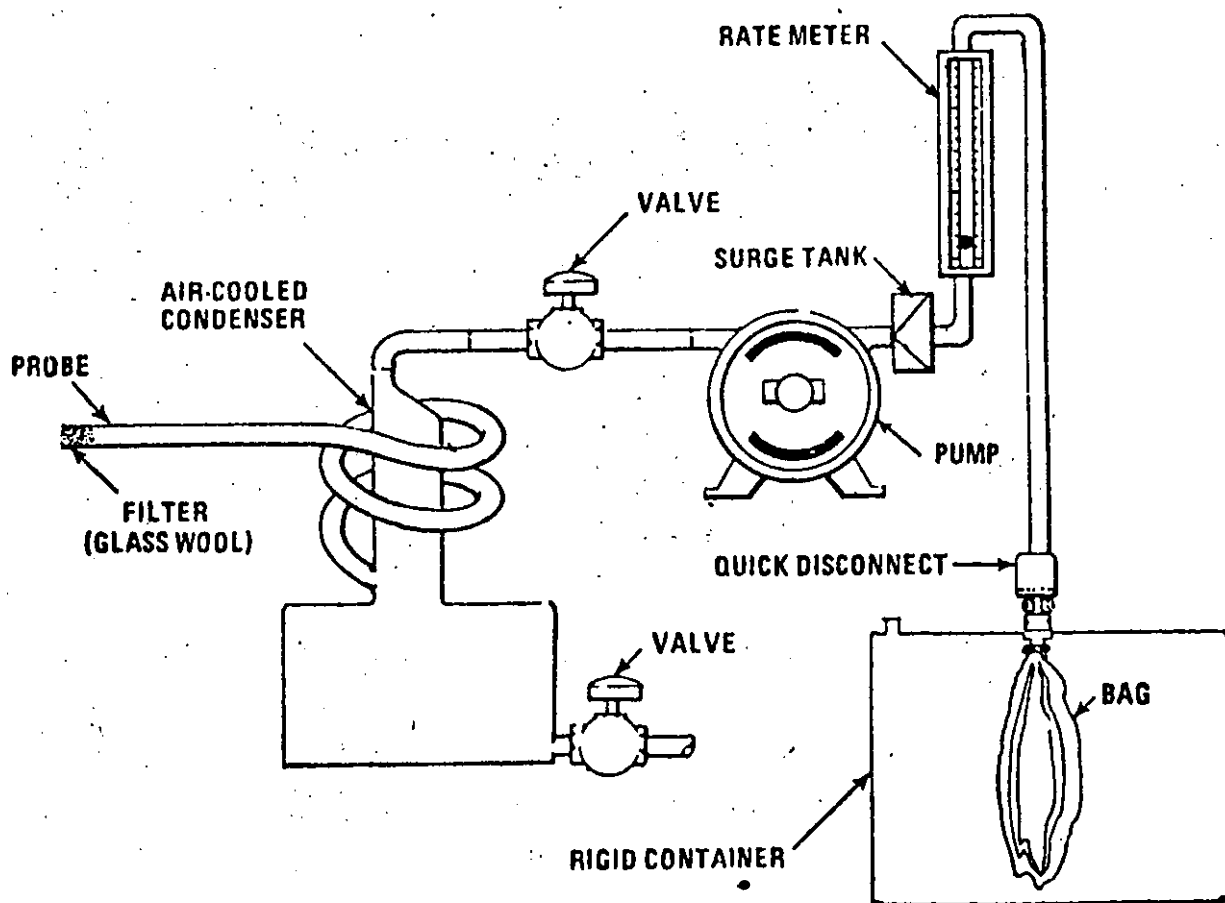


Figure 3-2. Integrated gas-sampling train.



than (a) 0.3 percent by volume when  $O_2$  is less than 15.0 percent or (b) 0.2 percent by volume when  $O_2$  is greater than 15.0 percent. Average the three acceptable values of percent  $O_2$  and report the results to the nearest 0.1 percent.

4.2.6.3 For percent  $CO$ , repeat the analytical procedure until the results of any three analyses differ by no more than 0.3 percent. Average the three acceptable values of percent  $CO$  and report the results to the nearest 0.1 percent.

4.2.7 After the analysis is completed, leak-check (annulater) the Orsat analyzer once again, as described in Section 6. For the results of the analysis to be valid, the Orsat analyzer must pass this leak test before and after the analysis. Note: Although in most instances only  $CO_2$  or  $O_2$  is required, it is recommended that both  $CO_2$  and  $O_2$  be measured, and that Citation 5 in the Bibliography be used to validate the analytical data.

4.3 Multi-Point, Integrated Sampling and Analytical Procedure.

4.3.1 Both the minimum number of sampling points and the sampling point location shall be as specified in Section 3.3.1 of this method. The use of fewer points than specified is subject to the approval of the Administrator.

4.3.2 Follow the procedures outlined in Sections 4.2.2 through 4.2.7, except for the following: Traverse all sampling points and sample at each point for an equal length of time. Record sampling data as shown in Figure 3-3.

### 6. Leak-Check Procedure for Orsat Analyzers

Moving an Orsat analyzer frequently causes it to leak. Therefore, an Orsat analyzer should be thoroughly leak-checked on site before the fine gas sample is introduced into it. The procedure for leak-checking an Orsat analyzer is:

6.1.1 Bring the liquid level in each pipette up to the reference mark on the capillary tubing and then close the pipette stopcock.

6.1.2 Raise the leveling bulb sufficiently to bring the confining liquid meniscus onto the graduated portion of the burette and then close the manifold stopcock.

6.1.3 Record the meniscus position.

6.1.4 Observe the meniscus in the burette and the liquid level in the pipette for movement over the next 4 minutes.

6.1.5 For the Orsat analyzer to pass the leak-check, two conditions must be met.

6.1.5.1 The liquid level in each pipette must not fall below the bottom of the capillary tubing during this 4-minute interval.

6.1.5.2 The meniscus in the burette must not change by more than 0.2 ml during this 4-minute interval.

6.1.6 If the analyzer fails the leak-check procedure, all rubber connections and stopcocks should be checked until the cause of the leak is identified. Leaking stopcocks must be disassembled, cleaned, and regreased. Leaking rubber connections must be replaced. After the analyzer is reassembled, the leak-check procedure must be repeated.

### 6. Calculations

#### 6.1. Noncombustibles.

$M_2$  - Dry molecular weight, g/g-mole (lb/lb-mole).

$\%EA$  - Percent excess air.

$\%CO_2$  - Percent  $CO_2$  by volume (dry basis).

$\%CO$  - Percent  $CO$  by volume (dry basis).

$\%O_2$  - Percent  $O_2$  by volume (dry basis).

$\%N_2$  - Percent  $N_2$  by volume (dry basis).

$\%H_2O$  - Ratio of  $O_2$  to  $N_2$  in air, v/v.

0.291 - Molecular weight of  $N_2$  or  $CO$ , divided by 100.

0.250 - Molecular weight of  $O_2$ , divided by 100.

0.440 - Molecular weight of  $CO_2$ , divided by 100.

6.2 Percent Excess Air. Calculate the percent excess air, if applicable, by substituting the appropriate values of percent  $O_2$ ,  $CO$ , and  $N_2$  obtained from Section 4.1.2 or 4.1.3 into Equation 3-1.

$$\%EA = \left[ \frac{\%O_2 - 0.5\%CO}{0.291\%N_2 (\%O_2 - 0.5\%CO)} \right] 100$$

Equation 3-1

Note.—The equation above assumes that ambient air is used as the source of  $O_2$  and that the fuel does not contain appreciable amounts of  $N_2$  (as do coke oven or blast furnace gases). For these cases when appreciable amounts of  $N_2$  are present (coal, oil, and natural gas do not contain appreciable amounts of  $N_2$ ) or when oxygen enrichment is used, alternate methods, subject to approval of the Administrator, are required.

6.3 Dry Molecular Weight. Use Equation 3-2 to calculate the dry molecular weight of the stack gas.

$$M_2 = 40(\%CO_2) + 0.29(\%CO) + 0.280(\%N_2 + \%CO)$$

Equation 3-2

Note.—The above equation does not consider argon in air (about 0.9 percent, molecular weight of 39.9). A negative error of about 0.4 percent is introduced. The tester may opt to include argon in the analysis using procedures subject to approval of the Administrator.

### 7. Bibliography

1. Altshuler, A. P. Storage of Gases and Vapors in Plastic Bags. *International Journal of Air and Water Pollution*, 6:75-81, 1963.

2. Conner, William D. and J. S. Nader. Air Sampling Plastic Bags. *Journal of the American Industrial Hygiene Association*, 22:291-297, 1961.

3. *Burrell Manual for Gas Analyzers*, Seventh edition, Burrell Corporation, 2223 Fifth Avenue, Pittsburgh, Pa. 15209, 1955.

4. Mitchell, W. J. and M. R. Mudgett. Field Reliability of the Orsat Analyzer. *Journal of Air Pollution Control Association* 20:191-195, May 1970.

5. Singhara, R. T., R. M. Neufeld, and W. S. Smith. Validating Orsat Analysis Data from Fossil Fuel-Fired Units. *Stack Sampling News*, 3(2):21-26, August, 1970.

### METHOD 4—DETERMINATION OF MOISTURE CONTENT IN STACK GASES

#### 1. Principle and Applicability

1.1 Principle. A gas sample is extracted at a constant rate from the source, moisture is removed from the sample stream and determined either volumetrically or gravimetrically.

1.2 Applicability. This method is applicable for determining the moisture content of stack gas.

Two procedures are given. The first is a reference method, for accurate determinations of moisture content of such as are needed in calculate emission data. The second is an approximation method, which provides estimates of percent moisture in air in setting lock-in sampling rates prior to a pollutant emission measurement run. The approximation method described herein is only a suggested approach; alternative means for approximating the moisture content, e.g., drying tubes, wet bulb-dry bulb techniques, condensation techniques, stoichiometric calculations, previous experience, etc., are also acceptable.

The reference method is often conducted simultaneously with a pollutant emission measurement run; when it is, calculation of percent isokinesis, pollutant emission rate, etc., for the run shall be based upon the results of the reference method or its equivalent. These calculations shall not be based upon the results of the approximation method, unless the approximation method is shown, to the satisfaction of the Administrator, U.S. Environmental Protection Agency, to be capable of yielding results within 1 percent (1:1) of the reference method.

Note.—The reference method may yield questionable results when applied to saturated gas streams or to streams that contain water droplets. Therefore, when these conditions exist or are suspected, a second determination of the moisture content shall be made simultaneously with the reference method, as follows: Assume that the gas stream is saturated. Attach a temperature sensor capable of measuring to  $\pm 1^\circ C$  ( $\pm 2^\circ F$ ) to the reference method probe. Measure the stack gas temperature at each traverse point (see Section 2.2.1) during the reference method traverse; calculate the average stack gas temperature. Next, determine the moisture percentage, either by: (1) using a psychrometric chart and making appropriate corrections if stack pressure is different from that of the chart, or (2) using saturation vapor pressure tables. In cases where the psychrometric chart or the saturation vapor pressure tables are not applicable (based on evaluation of the process), alternate methods, subject to the approval of the Administrator, shall be used.

#### 2. Reference Method

The procedure described in Method 5 for determining moisture content is acceptable as a reference method.

2.1 Apparatus. A schematic of the sampling train used in this reference method is shown in Figure 4.1. All components shall be maintained and calibrated according to the procedure outlined in Method 5.

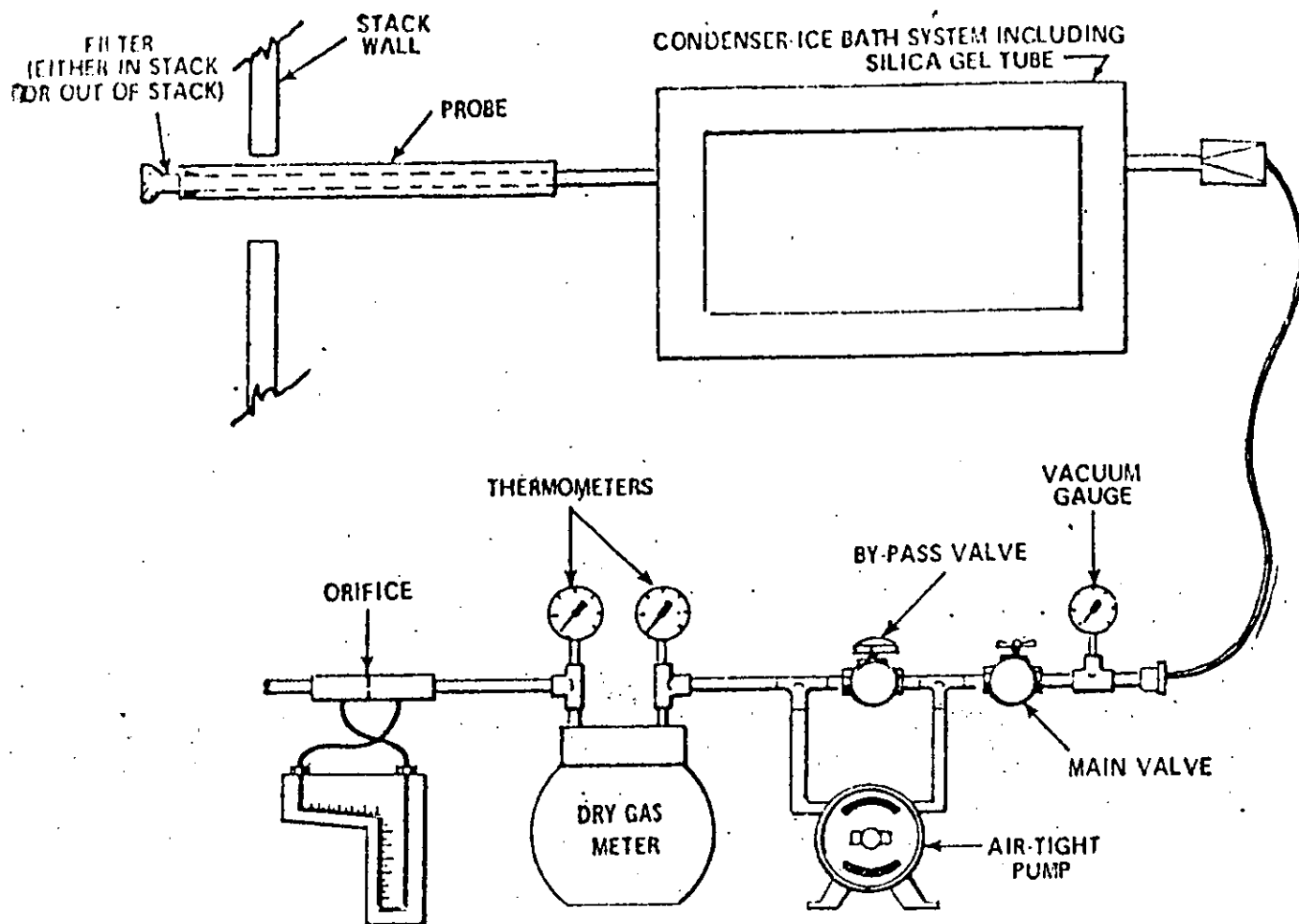


Figure 4-J. Moisture sampling train-reference method.

2.1.1 **Probe.** The probe is constructed of stainless steel or glass tubing, sufficiently heated to prevent water condensation, and is equipped with a filter, either in-stack (e.g., a plug of glass wool inserted into the end of the probe) or heated out-stack (e.g., as described in Method 5), to remove particulate matter.

When stack conditions permit, other metals or plastic tubing may be used for the probe, subject to the approval of the Administrator.

2.1.2 **Condenser.** The condenser consists of four impingers connected in series with ground glass, leak-free fittings or any similarly leak-free non-contaminating fittings. The first, third, and fourth impingers shall be of the Greenburg-Smith design, modified by replacing the top with a 1.3 centimeter (1/2 inch) ID glass tube extending to about 1.3 cm (1/2 in.) from the bottom of the flask. The second impinger shall be of the Greenburg-Smith design with the standard tip. Modifications (e.g., using flexible connections between the impingers, using materials other than glass, or using desiccable vacuum lines to connect the filter holder to the condenser) may be used, subject to the approval of the Administrator.

The first two impingers shall contain known volumes of water, the third shall be empty, and the fourth shall contain a known weight of 6 to 10-mesh indulating type silica gel, or equivalent desiccant. If the silica gel has been previously used, dry at 125° C (257° F) for 2 hours. New silica gel may be used as received. A thermometer, capable of measuring temperature to within 1° C (2° F), shall be placed at the outlet of the fourth impinger, for monitoring purposes.

Alternatively, any system may be used (subject to the approval of the Administrator) that cools the sample gas stream and allows measurement of both the water that has been condensed and the moisture leaving the condenser, such as within 1 ml or 1 µl. Acceptable means are to measure the condensed water, either gravimetrically or volumetrically, and to measure the moisture leaving the condenser by: (1) monitoring the barometric pressure at the exit of the condenser and using Dalton's law of partial pressures, or (2) passing

the sample gas stream through a tared silica gel (or equivalent desiccant) trap, with exit gases kept below 20° C (68° F), and determining the weight gain.

If means other than silica gel are used to determine the amount of moisture leaving the condenser, it is recommended that silica gel (or equivalent) still be used between the condenser system and pump, to prevent moisture condensation in the pump and metering devices and to avoid the need to make corrections for moisture in the metered volume.

2.1.3 **Cooling System.** An ice bath container and crushed ice (or equivalent) are used to aid in condensing moisture.

2.1.4 **Metering System.** This system includes a vacuum gauge, leak-free pump, thermometers capable of measuring temperature to within 3° C (45° F), dry gas meter capable of measuring volume to within 2 percent, and related equipment as shown in Figure 4-J. Other metering systems, capable of maintaining a constant sampling rate and determining sample gas volume, may be used, subject to the approval of the Administrator.

2.1.5 **Barometer.** Mercury, aneroid, or other barometer capable of measuring atmospheric pressure to within 2.5 mm Hg (0.1 in. Hg) may be used. In many cases, the barometric reading may be obtained from a nearby national weather service station, in which case the station value (which is the absolute barometric pressure) shall be requested and an adjustment for elevation difference between the weather station and the sampling point shall be applied at a rate of minus 2.5 mm Hg (0.1 in. Hg) per 30 m (100 ft) elevation increase or vice versa for elevation decrease.

2.1.6 **Graduated Cylinder and/or Balance.** These items are used to measure condensed water and moisture caught in the silica gel to within 1 ml or 0.5 g. Graduated cylinders shall have subdivisions no greater than 2 ml. Most laboratory balances are capable of weighing to the nearest 0.5 g or less. These balances are suitable for use here.

2.2 **Procedure.** The following procedure is written for a condenser system (such as the impinger system de-

scribed in Section 2.1.2) incorporating volumetric analysis to measure the condensed moisture, and silica gel and gravimetric analysis to measure the moisture leaving the condenser.

2.2.1 Unless otherwise specified by the Administrator, a minimum of eight traverse points shall be used for circular stacks having diameters less than 0.61 m (24 in.), a minimum of nine points shall be used for rectangular stacks having equivalent diameters less than 0.61 m (24 in.), and a minimum of twelve traverse points shall be used in all other cases. The traverse points shall be located according to Method 1. The use of fewer points is subject to the approval of the Administrator. Select a suitable probe and probe length such that all traverse points can be sampled. Consider sampling from opposite sides of the stack (four total sampling ports) for large stacks, to permit use of shorter probe lengths. Mark the probe with heat resistant tape or by some other method to denote the proper distance into the stack or duct for each sampling point. Then known volumes of water in the first two impingers. Weigh and record the weight of the silica gel to the nearest 0.5 g, and transfer the silica gel to the fourth impinger; alternatively, the silica gel may first be transferred to the impinger, and the weight of the silica gel plus impinger recorded.

2.2.2 Select a total sampling time such that a minimum total gas volume of 0.025 m<sup>3</sup> (21 scf) will be collected, at a rate no greater than 0.01 m<sup>3</sup>/min (0.75 cfm). When both moisture content and pollutant emission rate are to be determined, the moisture determination shall be simultaneous with, and for the same total length of time as, the pollutant emission rate run, unless otherwise specified in an applicable subpart of the standards.

2.2.3 Set up the sampling train as shown in Figure 4-J. Turn on the probe heater and (if applicable) the filter heating system to temperatures of about 125° C (255° F), to prevent water condensation ahead of the condenser; allow time for the temperatures to stabilize. Place crushed ice in the ice bath container. It is recommended, but not required, that a leak check be done, as follows: Disconnect the probe from the first impinger or



2.2 b. After collecting the sample, disconnect the probe from the filter holder (or from the first impinger) and conduct a leak check (mandatory) as described in Section

[illegible]

Figure 4-2. Field moisture determination-reference method.

|            | IMPIINGER<br>VOLUME,<br>ml | SILICA GEL<br>WEIGHT,<br>g |
|------------|----------------------------|----------------------------|
| FINAL      |                            |                            |
| INITIAL    |                            |                            |
| DIFFERENCE |                            |                            |

Figure 4.3. Analytical data—reference method.

## 2.3.1 Nomenclature:

- $R_{H_2O}$  = Proportion of water vapor, by volume, in the gas stream.
- $M_{H_2O}$  = Molecular weight of water, 18.0 g/g-mole (18.0 lb/lb-mole).
- $P_{atm}$  = Absolute pressure (for this method, same as barometric pressure) at the dry gas meter, mm Hg (in. Hg).
- $P_{std}$  = Standard absolute pressure, 760 mm Hg (29.92 in. Hg).
- $R$  = Ideal gas constant, 0.08206 (mm Hg) (ml)/(g-mole) (°K) for metric units and 21.85 (in. Hg) (ft<sup>3</sup>)/(lb-mole) (°R) for English units.
- $T_{atm}$  = Absolute temperature at meter, °K (°F).
- $T_{std}$  = Standard absolute temperature, 293° K (528° R).
- $V_{dm}$  = Dry gas volume measured by dry gas meter, dm (ft<sup>3</sup>).
- $\Delta V_{dm}$  = Incremental dry gas volume measured by dry gas meter at each traverse point, dm (ft<sup>3</sup>).
- $V_{dm, std}$  = Dry gas volume measured by the dry gas meter, corrected to standard conditions, dm (ft<sup>3</sup>).
- $V_{w, std}$  = Volume of water vapor condensed corrected to standard conditions, cm (in.).
- $V_{w, coll}$  = Volume of water vapor collected in silica gel corrected to standard conditions, cm (in.).
- $V_c$  = Final volume of condenser water, ml.
- $V_i$  = Initial volume, if any, of condenser water, ml.
- $W_c$  = Final weight of silica gel or silica gel plus impinger, g.
- $W_i$  = Initial weight of silica gel or silica gel plus impinger, g.
- $Y$  = Dry gas meter calibration factor.
- $\rho_w$  = Density of water, 0.9982 g/ml (0.0239 lb/in<sup>3</sup>).

## 2.3.2 Volume of water vapor condensed.

$$V_{w, coll} = \frac{(V_f - V_i) \rho_w R T_{atm}}{P_{atm} M_{H_2O}}$$

$$= K_1 (V_f - V_i)$$

where:

$K_1 = 0.001353$  ml/ml for metric units  
 $= 0.04707$  ft<sup>3</sup>/ml for English units

## 2.3.3 Volume of water vapor collected in silica gel.

$$V_{w, coll} = \frac{(W_f - W_i) R T_{atm}}{P_{atm} M_{H_2O}}$$

$$= K_2 (W_f - W_i)$$

where:

$K_2 = 0.001353$  ml/g for metric units  
 $= 0.04716$  ft<sup>3</sup>/g for English units

## 2.3.4 Sample gas volume.

$$V_{s, coll} = V_{dm} Y \frac{(P_{atm})(T_{std})}{(P_{coll})(T_{atm})}$$

$$= K_3 Y \frac{P_{atm}}{T_{atm}}$$

Equation 4.3

where:

$K_3 = 0.3658$  K/mm Hg, for metric units  
 $= 0.0118$  R/in. Hg for English units

Note: If the post-test leak rate (Section 2.2c) exceeds the allowable rate, correct the value of  $V_{dm}$  in Equation 4.3, as described in Section 6.3 of Method 5.

## 2.3.5 Moisture Content.

$$B_{H_2O} = \frac{V_{w, coll} + V_{w, std}}{V_{s, coll} + V_{s, std} + V_{dm, std}}$$

Equation 4.4

Note:—In saturated or moisture droplet-laden gas streams, two calculations of the moisture content of the stack gas shall be made, one using a value based upon the saturated conditions (see Section 1.2), and another based upon the results of the impinger analysis. The lower of these two values of  $B_{H_2O}$  shall be considered correct.

2.3.6 Verification of constant sampling rate. For each time increment, determine the  $\Delta V_{dm}$ . Calculate the average. If the value for any time increment differs from the average by more than 10 percent, reject the results and repeat the run.

## 3. Approximation Method

The approximation method described below is presented only as a suggested method (see Section 1.2).

## 3.1 Apparatus.

3.1.1 Probe: Stainless steel or glass tubing, sufficiently heated to prevent water condensation and equipped with a filter (either in-stack or located out-stack) to remove particulate matter. A plug of glass wool, inserted into the end of the probe, is a satisfactory filter.

3.1.2 Impingers: Two midjet impingers, each with 30 ml capacity, or equivalent.

3.1.3 Ice Bath: Container and ice, to aid in condensing moisture in impingers.

3.1.4 Dryer: Tube, Tube packed with new or regenerated 6- to 16-mesh ind-act-type silica gel (or equivalent desiccant), to dry the sample gas and to protect the meter and pump.

3.1.5 Valve: Needle valve, to regulate the sample gas flow rate.

3.1.6 Pump: Leak-free, diaphragm type, or equivalent, to pull the gas sample through the train.

3.1.7 Volume meter: Dry gas meter, sufficiently accurate to measure the sample volume within 2%, and calibrated over the range of flow rates and conditions actually encountered during sampling.

3.1.8 Flow Meter: Rotameter, to measure the flow range from 0 to 3 lpm (0 to 0.11 cfm).

3.1.9 Graduated Cylinder: 25 ml.

3.1.10 Barometer: Mercury, aneroid, or other barometer, as described in Section 2.1.5 above.

3.1.11 Vacuum Gauge: At least 760 mm Hg (30 in. Hg) gauge, to be used for the sampling leak check.

## 3.2 Procedure.

3.2.1 Place exactly 5 ml distilled water in each impinger. Assemble the apparatus without the probe as shown in Figure 4.4. Leak check the train by placing a vacuum gauge at the inlet to the first impinger and drawing a vacuum of at least 250 mm Hg (10 in. Hg), plugging the outlet of the rotameter, and then turning off the pump. The vacuum shall remain constant for at least one minute. Carefully release the vacuum gauge before uncoupling the rotameter end.

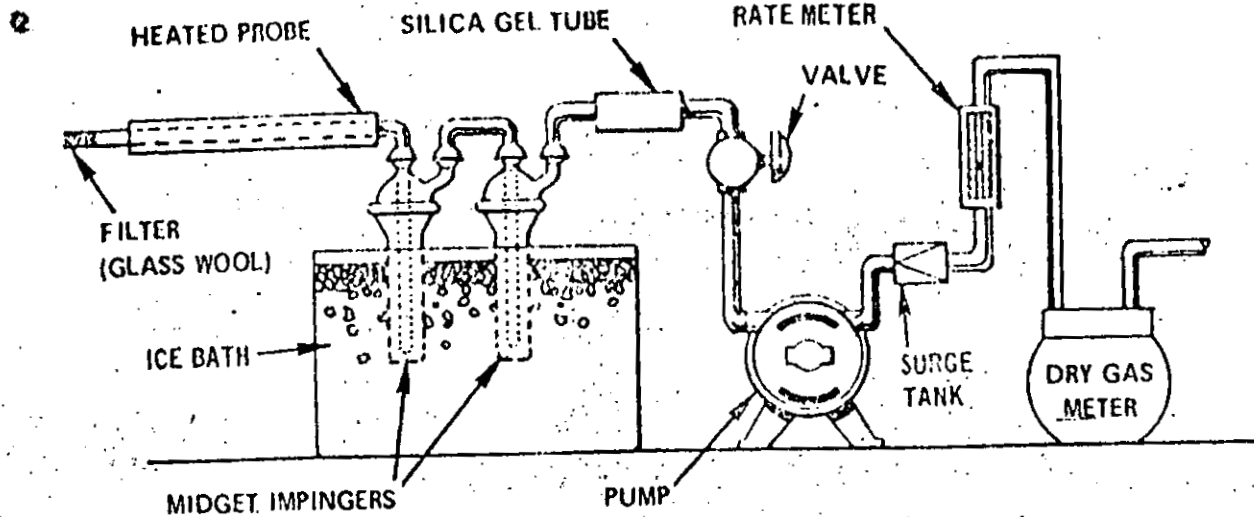


Figure 4-4. Moisture-sampling train - approximation method.

LOCATION \_\_\_\_\_ COMMENTS \_\_\_\_\_  
 TEST \_\_\_\_\_  
 DATE \_\_\_\_\_  
 OPERATOR \_\_\_\_\_  
 BAROMETRIC PRESSURE \_\_\_\_\_

| CLOCK TIME | GAS VOLUME THROUGH<br>METER, (Vm),<br>m <sup>3</sup> (ft <sup>3</sup> ) | RATE METER SETTING<br>m <sup>3</sup> /min. (ft <sup>3</sup> /min.) | METER TEMPERATURE,<br>°C (°F) |
|------------|-------------------------------------------------------------------------|--------------------------------------------------------------------|-------------------------------|
|            |                                                                         |                                                                    |                               |
|            |                                                                         |                                                                    |                               |
|            |                                                                         |                                                                    |                               |
|            |                                                                         |                                                                    |                               |
|            |                                                                         |                                                                    |                               |

Figure 4-5. Field moisture determination - approximation method.

3.2.2. Connect the probe, insert it into the stack, and sample at a constant rate of 2 lpm (0.071 cfm). Continue sampling until the dry gas meter registers about 90 liters (3.16) or until visible liquid droplets are carried over from the first impinger to the second. Record temperature, pressure, and dry gas meter readings as required by Figure 4-5.

3.2.3. After collecting the sample, combine the contents of the two impingers and measure the volume to the nearest 0.5 ml.

3.3. Calculations. The calculation method presented is designed to estimate the moisture in the stack gas; therefore, other data, which are only necessary for accurate moisture determinations, are not collected. The following equations adequately estimate the moisture content, for the purpose of determining isokinetic sampling rate settings.

#### 3.3.1. Nomenclature.

$B_{vol}$ —Approximate proportion, by volume, of water vapor in the gas stream leaving the second impinger, 0.025.

$B_{wt}$ —Water vapor in the gas stream, proportion by volume.

$M_w$ —Molecular weight of water, 18.0 g/g-mole (18.0 lb/lb-mole).

$P_a$ —Absolute pressure (for this method, same as barometric pressure) at the dry gas meter.

$P_{std}$ —Standard absolute pressure, 760 mm Hg (29.92 in. Hg).

$R$ —Ideal gas constant, 0.08206 (mm Hg) (m<sup>3</sup>)/(g-mole) (°K) for metric units and 31.85 (in. Hg) (ft<sup>3</sup>)/(lb-mole) (°R) for English units.

$T_a$ —Absolute temperature at meter, °K (°F).

$T_{std}$ —Standard absolute temperature, 293° K (62° R).

$V_i$ —Final volume of impinger contents, ml.

$V_{dry}$ —Initial volume of impinger contents, ml.

$V_{dry}$ —Dry gas volume measured by dry gas meter, dm (dm).

$V_{dry}(std)$ —Dry gas volume measured by dry gas meter, corrected to standard conditions, dm (dm).

$V_{w}(std)$ —Volume of water vapor condensed, corrected to standard conditions, scm (scf).

$\rho_w$ —Density of water, 0.9982 g/ml (0.00261 lb/ml).

#### 3.3.2. Volume of water vapor collected.

$$V_{w}(std) = \frac{(V_i - V_{dry}) \rho_w RT_{std}}{P_{std} M_w} \\ = K_1 (V_i - V_{dry})$$

Equation 4-5

where:

$K_1$ —0.001333 m<sup>3</sup>/ml for metric units

= 0.04707 ft<sup>3</sup>/ml for English units.

#### 3.3.3. Gas volume.

$$V_{dry}(std) = V_{dry} \left( \frac{P_a}{P_{std}} \right) \left( \frac{T_{std}}{T_a} \right) \\ = K_2 \frac{V_{dry} P_a}{T_a}$$

Equation 4-6

where:

$K_2$ —0.3858 °K/mm Hg for metric units

= 17.04 °R/in. Hg for English units

#### 3.3.4. Approximate moisture content.

$$B_{vol} = \frac{V_{w}(std)}{V_{w}(std) + V_{dry}(std)} + B_{wt} \\ = \frac{V_{w}(std)}{V_{w}(std) + V_{dry}(std)} + (0.025)$$

Equation 4-7

#### 4. Calibration

4.1. For the reference method, calibrate equipment as specified in the following sections of Method 5: Section 5.3 (metering system); Section 5.5 (temperature gauge); and Section 5.7 (barometer). The recommended leak check of the metering system (Section 5.6 of Method 5) also applies to the reference method. For the approximation method, use the procedures outlined in Section 5.1.1 of Method 5 to calibrate the metering system, and the procedure of Method 5, Section 5.7 to calibrate the barometer.

#### 5. Bibliography

1. Air Pollution Engineering Manual (Second Edition). Danielson, J. A. (ed.). U.S. Environmental Protection Agency, Office of Air Quality Planning and Standards, Research Triangle Park, N.C. Publication No. AP-40, 1973.

2. Deverekin, Howard, et al. Air Pollution Source Testing Manual. Air Pollution Control District, Los Angeles, Calif. November, 1963.

3. Methods for Determination of Velocity, Volume, Dust and Mist Content of Gases. Western Precipitation Division of Joy Manufacturing Co., Los Angeles, Calif. Bulletin WP-50, 1968.

#### METHOD 5—DETERMINATION OF PARTICULATE EMISSIONS FROM STATIONARY SOURCES

##### 1. Principle and Applicability

1.1. Principle. Particulate matter is withdrawn isokinetically from the source and collected on a glass fiber filter maintained at a temperature in the range of 120±14° C (248±25° F) or such other temperature as specified by an applicable subpart of the standards or approved by the Administrator, U.S. Environmental Protection Agency, for a particular application. The particulate mass, which includes any material that condenses at or above the filtration temperature, is determined gravimetrically after removal of uncombined water.

1.2. Applicability. This method is applicable for the determination of particulate emissions from stationary sources.

##### 2. Apparatus

2.1. Sampling Train. A schematic of the sampling train used in this method is shown in Figure 5-1. Complete construction details are given in APTD-0581 (Citation 2 in Section 7); commercial models of this train are also available. For changes from APTD-0581 and for allowable modifications of the train shown in Figure 5-1, see the following subsections.

The operating and maintenance procedures for the sampling train are described in APTD-0576 (Citation 3 in Section 7). Since correct usage is important in obtaining valid results, all users should read APTD-0576 and adopt the operating and maintenance procedures outlined in it, unless otherwise specified herein. The sampling train consists of the following components:

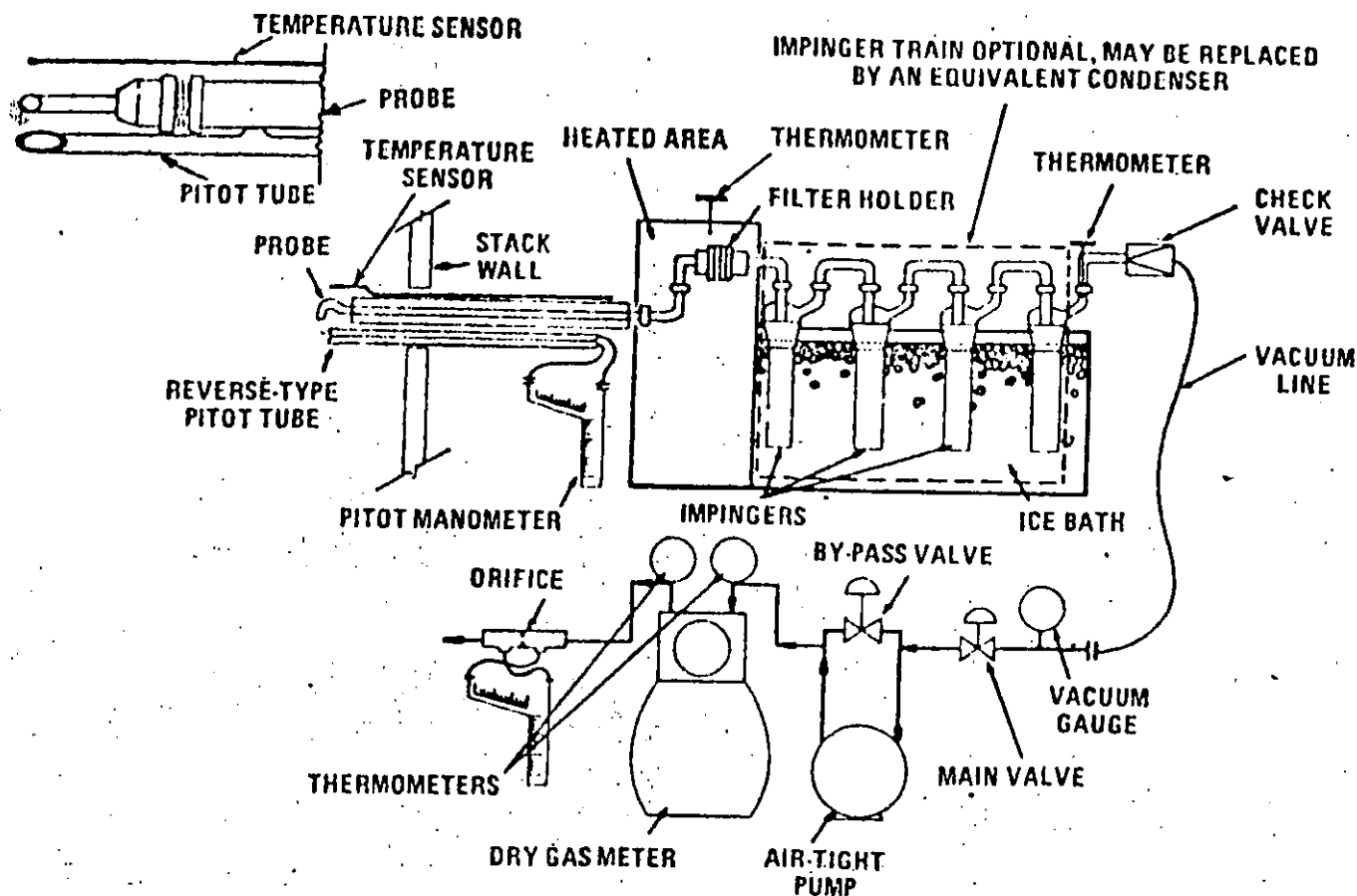


Figure 5-1. Particulate-sampling train.

2.1.1 Probe Nozzle. Stainless steel (316) or glass with sharp, tapered leading edge. The angle of taper shall be  $\leq 30^\circ$  and the taper shall be on the outside to preserve a constant internal diameter. The probe nozzle shall be of the button-hook or elbow design, unless otherwise specified by the Administrator. If made of stainless steel, the nozzle shall be constructed from seamless tubing; other materials of construction may be used, subject to the approval of the Administrator.

A range of nozzle sizes suitable for isokinetic sampling should be available, e.g., 0.32 to 1.27 cm (1/8 to 1/2 in.) or larger if higher volume sampling trains are used—inside diameter (ID) nozzles in increments of 0.16 cm (5/16 in.). Each nozzle shall be calibrated according to the procedures outlined in Section 5.

2.1.2 Probe Liner. Borosilicate or quartz glass tubing with a heating system capable of maintaining a gas temperature at the exit end during sampling of  $120 \pm 14^\circ \text{C}$  ( $248 \pm 25^\circ \text{F}$ ), or such other temperature as specified by an applicable subpart of the standards or approved by the Administrator for a particular application. (The heater may opt to operate the equipment at a temperature lower than that specified.) Since the actual temperature at the outlet of the probe is not usually monitored during sampling, probes constructed according to APTD-0581 and utilizing the calibration curves of APTD-0570 (or calibrated according to the procedure outlined in APTD-0570) will be considered acceptable.

Either borosilicate or quartz glass probe liners may be used for stack temperatures up to about  $180^\circ \text{C}$  ( $350^\circ \text{F}$ ); quartz liners shall be used for temperatures between  $180$  and  $315^\circ \text{C}$  ( $350$  and  $600^\circ \text{F}$ ). Both types of liners may be used at higher temperatures than specified for short periods of time, subject to the approval of the Administrator. The cooling temperature for borosilicate is  $15^\circ \text{C}$  ( $59^\circ \text{F}$ ), and for quartz it is  $1,340^\circ \text{C}$  ( $2,422^\circ \text{F}$ ).

Whenever practical, every effort should be made to use borosilicate or quartz glass probe liners. Alternatively, a seal liner (e.g., 316 stainless steel, Inconel 600, or other material resistant to acids) made of seamless tubing may be used, subject to the approval of the Administrator.

2.1.3 Pitot Tube. Type A, as described in Section 2.1 of Method 2, or other device approved by the Administrator. The pitot tube shall be attached to the probe (as shown in Figure 5-1) to allow constant monitoring of the gas velocity. The impact (high pressure) opening

plane of the pitot tube shall be even with or above the nozzle entry plane (see Method 2, Figure 2-6b) during sampling. The Type A pitot tube assembly shall have a known coefficient, determined as outlined in Section 4 of Method 2.

2.1.4 Differential Pressure Gauge. Inclined manometer or equivalent device (two), as described in Section 2.2 of Method 2. One manometer may be used for velocity head ( $\Delta p$ ) readings, and the other, for orifice differential pressure readings.

2.1.5 Filter Holder. Borosilicate glass, with a glass frit filter support and a silicone rubber gasket. Other materials of construction (e.g., stainless steel, Teflon, Viton) may be used, subject to approval of the Administrator. The holder design shall provide a positive seal against leakage from the outside or around the filter. The holder shall be attached immediately at the outlet of the probe (or cyclone, if used).

2.1.6 Filter Heating System. Any heating system capable of maintaining a temperature around the filter holder during sampling of  $120 \pm 14^\circ \text{C}$  ( $248 \pm 25^\circ \text{F}$ ), or such other temperature as specified by an applicable subpart of the standards or approved by the Administrator for a particular application. Alternatively, the heater may opt to operate the equipment at a temperature lower than that specified. A temperature gauge capable of measuring temperature to within  $3^\circ \text{C}$  ( $5.4^\circ \text{F}$ ) shall be installed so that the temperature around the filter holder can be regulated and monitored during sampling. Heating systems other than the one shown in APTD-0581 may be used.

2.1.7 Condenser. The following system shall be used to determine the stack gas moisture content: Four impingers connected in series with leak-free ground glass fittings or other similar leak-free non-contaminating fittings. The first, third, and fourth impingers shall be of the Greenburg-Smith design, modified by replacing the tip with 1.3 cm (1/2 in.) ID glass tube extending to about 1.3 cm (1/2 in.) from the bottom of the flask. The second impinger shall be of the Greenburg-Smith design with the standard tip. Modifications (e.g., using flexible connections between the impingers, using materials other than glass, or using flexible vacuum lines to connect the filter holder to the condenser) may be used, subject to the approval of the Administrator. The first and second impingers shall contain known quantities of water (Section 4.3.3), the third shall be empty, and the fourth shall contain a known weight of silica gel, or equivalent desiccant. A thermometer, capable of measuring temperature to within  $1^\circ \text{C}$  ( $2^\circ \text{F}$ ) shall be placed at the outlet of the fourth impinger for monitoring purposes.

Alternatively, any system that cools the sample gas stream and allows measurement of the water condensed and moisture leaving the condenser, each to within 1 ml or 1 g may be used, subject to the approval of the Administrator. Acceptable means are to measure the condensed water either gravimetrically or volumetrically and to measure the moisture leaving the condenser by: (1) monitoring the temperature and pressure at the exit of the condenser and using Dalton's law of partial pressures; or (2) passing the sample gas stream through a tared silica gel (or equivalent desiccant) trap with exit gases kept below  $20^\circ \text{C}$  ( $68^\circ \text{F}$ ) and determining the weight gain.

If means other than silica gel are used to determine the amount of moisture leaving the condenser, it is recommended that silica gel (or equivalent) shall be used between the condenser system and pump to prevent moisture condensation in the pump and metering devices and to avoid the need to make corrections for moisture in the material volume.

NOTE.—If a determination of the particulate matter collected in the impingers is desired in addition to moisture content, the impinger system described above shall be used, without modification. Individuals, States, or control agencies requiring this information shall be contacted as to the sample recovery and analysis of the impinger contents.

2.1.8 Metering System. Vacuum gauge, leak-free pump, thermometers capable of measuring temperature to within  $3^\circ \text{C}$  ( $5.4^\circ \text{F}$ ), dry gas meter capable of measuring volume to within 2 percent, and related equipment, as shown in Figure 5-1. Other metering systems capable of maintaining sampling rates within 10 percent of isokinetic and of determining sample volumes to within 2 percent may be used, subject to the approval of the Administrator. When the metering system is used in conjunction with a pitot tube, the system shall enable checks of isokinetic rates.

Sampling trains utilizing metering systems designed for higher flow rates than that described in APTD-0581 or APTD-0570 may be used provided that the specifications of this method are met.

2.1.9 Barometer. Mercury, aneroid, or other barometer capable of measuring atmospheric pressure to within  $2.5$  mm Hg ( $0.1$  in. Hg). In many cases, the barometric reading may be obtained from a nearby national weather service station, in which case the station value (which is

1. Mention of trade names or specific products does not constitute endorsement by the Environmental Protection Agency.



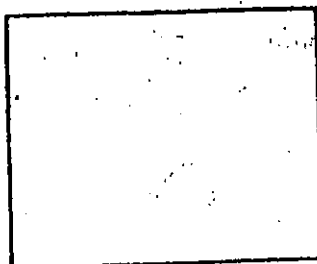
## RULES AND REGULATIONS

Take other readings required by Figure 5-2 at least once at each sample point during each time increment and additional readings when significant changes (20 percent variation in velocity head readings) necessitate additional adjustments in flow rate. Level and zero may drift due to vibratory and temperature changes, make periodic checks during the traverse.

Given the portholes prior to the test run to minimize the chance of sampling deposited material. To begin sampling, remove the sample cap, verify that the filter and probe heating systems are up to temperature, and that the pump lines and probe are properly positioned. Position the manifold at the first traverse point with the probe pointing directly into the gas stream. Immediate conditions at the pump and adjust the flow to lock-in the conditions. Nomenclature is available, which aid in the rapid adjust-

ment of the lookinodic measuring rate without excessive computations. These nomographs are designed for use when the Type B pilot tube coefficient is 0.85-1.00, and the stack gas equivalent density (dry molecular weight) is equal to 24.4. A 10% density deviation is permissible using the nomographs. If  $C_p$  and  $M_g$  are outside these stated ranges do not use the nomographs unless appropriate steps (see Section 7 in Section 7) are taken to compensate for the deviations.

PLANT \_\_\_\_\_  
LOCATION \_\_\_\_\_  
OPERATOR \_\_\_\_\_  
DATE \_\_\_\_\_  
RUN NO. \_\_\_\_\_  
SAMPLE BOX NO. \_\_\_\_\_  
METER BOX NO. \_\_\_\_\_  
METER  $\Delta H_0$  \_\_\_\_\_  
C FACTOR \_\_\_\_\_  
PITOT TUBE COEFFICIENT,  $C_p$  \_\_\_\_\_



**SCHEMATIC OF STACK CROSS SECTION**

AMBIENT TEMPERATURE \_\_\_\_\_  
 BAROMETRIC PRESSURE \_\_\_\_\_  
 ASSUMED MOISTURE, % \_\_\_\_\_  
 PROBE LENGTH, m (ft) \_\_\_\_\_  
 NOZZLE IDENTIFICATION NO. \_\_\_\_\_  
 AVERAGE CALIBRATED NOZZLE DIAMETER, cm (in.) \_\_\_\_\_  
 PROBE HEATER SETTING \_\_\_\_\_  
 LEAK RATE, m<sup>3</sup>/min. (cfm) \_\_\_\_\_  
 PROBE LINER MATERIAL \_\_\_\_\_  
 STATIC PRESSURE, mm Hg (in. Hg) \_\_\_\_\_  
 FILTER NO. \_\_\_\_\_

[illegible]

**Figure 5-2. Particulate field data.**

When the stack is under significant negative pressure (height of impinger stem), take care to close the coarse adjust valve before inserting the probe into the stack to prevent water from backing into the filter holder. If necessary, the pump may be turned on with the coarse adjust valve closed.

When the probe is in position, block off the openings around the probe and ports to prevent unrepresentative dilution of the gas stream.

Traverse the stack cross-section, as required by Method 1 or as specified by the Administrator, being careful not to bump the probe into the stack walls when sampling near the walls or when removing or inserting the probe through the portholes; this minimizes the chance of extracting deposited material.

During the test run, make periodic adjustments to keep the temperature around the filter holder at the proper level; add more ice and, if necessary, salt to maintain a temperature of less than 20° C (68° F) at the condenser/sink gel outlet. Also, periodically check the level and zero of the manometer.

If the pressure drop across the filter becomes too high, making isochroic sampling difficult to maintain, the filter may be replaced in the midst of a sample run. It is recommended that another complete filter assembly be used rather than attempting to change the filter itself. Once a new filter assembly is installed, conduct a bench test (see Section 4.1.4.2). The total particulate weight should be the summation of all three sequentially replaced filters.

A single train shall be used for the entire sample run. In cases where simultaneous sampling is required in two or more separate ducts or at two or more different stations within the same duct, or in cases where equipment failure necessitates a change of train, in all other instances, the use of two or more trains will be subject to the approval of the Administrator.

Note that when two or more trains are used, separate analysis of the front-hall and (if applicable) impinger catches from each train shall be performed, unless identical nozzle sizes were used on all trains, in which case, the front-hall catches from individual trains may be combined (as may the impinger catches) and one analysis of front-hall catch and one analysis of impinger catch may be performed. Consult with the Administrator for details concerning the calculation of results when two or more trains are used.

At the end of the sample run, turn off the coarse adjust valve, remove the probe and nozzle from the stack, turn off the pump, record the final dry gas meter reading, and conduct a post-test leak check, as outlined in Section 4.1.4.3. Also, leak-check the pilot lines as described in Method 2, Section 5.1; the lines must pass this leak-check, indicate the velocity head data.

4.1.0 Calculation of Percent Isokinetic. Calculate percent isokinetic (see Calculations, Section 8) to determine whether the run was valid or another test run should be made. If there was difficulty in maintaining isokinetic rates due to source conditions, consult with the Administrator for possible variance on the isokinetic rates.

4.2 **Sample Recovery.** Proper cleanup procedure begins as soon as the probe is removed from the stick at the end of the sampling period. Allow the probe to cool. When the probe can be safely handled, wipe off all external particulate matter near the tip of the probe nozzle and place a cover over it to prevent losing or gaining particulate matter. Do not rip off the probe tip tightly while the sampling train is cooling; down as this would create a vacuum in the filter holder, thus drawing water from the impinger into the filter holder. Before storing the sample train to the cleanup site, remove the probe from the sample train, wipe off the

silicone grease, and cap the open outlet of the probe. Be careful not to lose any condensate that might be present. Wipe off the silicone grease from the filter inlet where the probe was fastened and cap it. Remove the umbilical cord from the last impinger and cap the impinger. If a flexible line is used between the first impinger or condenser and the filter holder, disconnect the line at the filter holder and let any undrained water or liquid drain into the impinger or condenser. After wiping off the silicone grease, cap off the filter holder outlet and impinger inlet. Either ground-glass stoppers, plastic or aluminum caps may be used to close these openings.

Transfer the probe and filter-impinger assembly to the cleanup area. This area should be clean and protected from the wind so that the chances of contaminating or losing the sample will be minimized.

Save a portion of the acetone used for cleanup as a blank. Take 200 ml of this acetone directly from the wash bottle being used and place it in a glass sample container for the acetone blank.

Inspect the train prior to and during disassembly and note any abnormal conditions. Treat the samples as follows:

**Container No. 1.** Carefully remove the filter from the filter holder and place it in its identified petri dish container. Use a pair of tweezers and clean disposable surgical gloves to handle the filter. If it is necessary to fold the filter, do so such that the particulate cake is held in the fold. Carefully transfer to the petri dish any insoluble residue. Carefully transfer to the petri dish any particulate matter and/or filter fibers which adhere to the filter holder gasket, by using a dry nylon bristle brush and a plasticized blade. Seal the container. (The

Container No. 2. Taking care to see that it is on the outside of the probe or other exterior surface does not get into the sample, quantitatively recover particulate matter or any condensate from the probe nozzle, probe

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filter, probe filter, and front half of the filter holder by washing these components with acetone and placing the wash in a glass container. Distilled water may be used instead of acetone when approved by the Administrator and shall be used when specified by the Administrator; in these cases, make a white blank and follow the Administrator's directions on analysis. Perform the acetone rinses as follows:

1. Carefully remove the probe nozzle and clean the inside surface by shooting with acetone from a wash bottle and brushing with a nylon bristle brush. Brush until the acetone rinse shows no visible particles, after which make a final rinse of the inside surface with acetone.

2. Brush and rinse the inside parts of the impinger fitting with acetone in a similar way until no visible particles remain.

3. Rinse the probe filter with acetone by tilting and rotating the probe while squirting acetone into its upper end so that all inside surfaces will be wetted with acetone. Let the acetone drain from the lower end into the sample container. A funnel collar or polyethylene may be used to aid in transferring liquid wastes to the container. Follow the acetone rinse with a probe brush. Hold the probe in an inclined position, apply acetone into the upper end as the probe brush is being pushed with a twisting action through the probe; hold a sample container underneath the lower end of the probe, and catch any acetone and particulate matter which is brushed from the probe. Run the brush through the probe three times or more until no visible particulate matter is caught out with the acetone or until some remains in the probe liner on visual inspection. With stainless steel or other metal probes, run the brush through in the above prescribed manner at least six times since metal probes have small crevices in which particulate matter can be entrapped. Rinse the brush with acetone, and quantitatively collect these washings in the sample container. After the brushing, make a final acetone rinse of the probe as described above.

It is recommended that two people be used to clean the probe to minimize sample losses. Between sampling runs, keep brushes clean and protected from contamination.

After ensuring that all joints have been wiped clean of silicone grease, clean the inside of the front half of the filter holder by rubbing the surfaces with a nylon bristle brush and rinsing with acetone. Rinse each surface three times or more if needed to remove visible particulate. Make a final rinse of the brush and filter holder. Carefully rinse out the glass, yalene, also (if applicable). After all acetone washings and particulate matter have been collected in the sample container, tighten the lid on the sample container so that acetone will not leak out when it is shipped to the laboratory. Mark the height of the fluid level to determine whether or not leakage occurred during transport. Label the container to clearly identify its contents.

**Container No. 3.** Note the color of the indicating silica gel to determine if it has been completely spent and make a notation of its condition. Transfer the silica gel from the fourth impinger to its original container and seal. A funnel may make it easier to pour the silica gel without spilling. A rubber policeman may be used as an aid in removing the silica gel from the impinger. It is not necessary to remove the small amount of dust particles that may adhere to the impinger wall and are difficult to remove. Since the gain in weight is to be used for moisture calculations, do not use any water or other liquids to transfer the silica gel. If a balance is available in the field, follow the procedure for container No. 3 in Section 4.3.

**Impinger Water.** Treat the impingers as follows: Make a notation of any color or film in the liquid catch. Measure the liquid which is in the first three impingers to within  $\pm 1$  ml by using a graduated cylinder or by weighing it to within  $\pm 0.5$  g by using a balance (if one is available). Record the volume or weight of liquid present. This information is required to calculate the moisture content of the effluent gas.

Discard the liquid after measuring and recording the volume or weight, unless analysis of the impinger catch is required (see Note, Section 2.1.7).

If a different type of condenser is used, measure the amount of moisture condensed either volumetrically or gravimetrically.

Whenever possible, containers should be shipped in such a way that they remain upright at all times.

**4.3 Analysis.** Record the data required on a sheet such as the one shown in Figure 5-3. Handle each sample container as follows:

**Container No. 1.** Leave the contents in the shipping container or transfer the filter and any loose particulate from the sample container to a tared glass weighing dish. Desiccate for 24 hours in a desiccator containing anhydrous calcium sulfate. Weigh to a constant weight and report the results to the nearest 0.1 mg. For purposes of this Section, 4.3, the term "constant weight" means a difference of no more than 0.5 mg or 1 percent of total weight less tare weight, whichever is greater, between two consecutive weighings, with no less than 6 hours of desiccation time between weighings.

Plant \_\_\_\_\_

Date \_\_\_\_\_

Run No. \_\_\_\_\_

Filter No. \_\_\_\_\_

Amount liquid lost during transport \_\_\_\_\_

Acetone blank volume, ml \_\_\_\_\_

Acetone wash volume, ml \_\_\_\_\_

Acetone blank concentration, mg/mg (equation 5-4) \_\_\_\_\_

Acetone wash blank, mg (equation 5-5) \_\_\_\_\_

| CONTAINER NUMBER             | WEIGHT OF PARTICULATE COLLECTED, mg |             |             |
|------------------------------|-------------------------------------|-------------|-------------|
|                              | FINAL WEIGHT                        | TARE WEIGHT | WEIGHT GAIN |
| 1                            |                                     |             |             |
| 2                            |                                     |             |             |
| TOTAL                        |                                     |             |             |
| Less acetone blank           |                                     |             |             |
| Weight of particulate matter |                                     |             |             |

|                        | VOLUME OF LIQUID WATER COLLECTED |                      |
|------------------------|----------------------------------|----------------------|
|                        | IMPINGER VOLUME, ml              | SILICA GEL WEIGHT, g |
| FINAL                  |                                  |                      |
| INITIAL                |                                  |                      |
| LIQUID COLLECTED       |                                  |                      |
| TOTAL VOLUME COLLECTED |                                  | g <sup>a</sup> ml    |

- CONVERT WEIGHT OF WATER TO VOLUME BY DIVIDING TOTAL WEIGHT INCREASE BY DENSITY OF WATER (1g/ml).

$$\frac{\text{INCREASE, g}}{1 \text{ g/ml}} = \text{VOLUME WATER, ml}$$

Figure 5-3. Analytical data.



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Alternatively, the sample may be oven dried at 100° C (212° F) for 2 to 3 hours, cooled in the desiccator, and weighed to a constant weight, unless otherwise specified by the Administrator. The sample may also be oven dried at 100° C (212° F) for 2 to 3 hours, weighed, and use this weight as a final weight.

**Caution No. 2.** Note the level of liquid in the container and confirm on the Analysis sheet whether or not leakage occurred during transport. If a noticeable amount of leakage has occurred, either void the sample or use methods, subject to the approval of the Administrator, to correct the final results. Measure the liquid in this container either volumetrically to 0.1 ml or gravimetrically to 0.001 g. Transfer the contents to a tared 250-ml beaker and evaporate to dryness at ambient temperature and pressure. Desiccate for 24 hours and weigh to a constant weight. Report the results to the nearest 0.1 mg.

**Caution No. 3.** Weigh the spent drying gel (or silica gel plus impinger) to the nearest 0.5 g using a balance. This step may be conducted in the field.

**"Acetone Blank" Check.** Measure acetone in this container either volumetrically or gravimetrically. Transfer the acetone to a tared 250 ml beaker and evaporate to dryness at ambient temperature and pressure. Desiccate for 24 hours and weigh to a constant weight. Report the results to the nearest 0.1 mg.

**Note.**—At the option of the tester, the contents of Container No. 2 as well as the acetone blank container may be evaporated at temperatures higher than ambient, if evaporation is done at an elevated temperature, the temperature must be below the boiling point of the solvent; also, to prevent "bumping," the evaporation process must be closely supervised, and the contents of the beaker must be stirred occasionally to maintain an even temperature. Use extreme care, as acetone is highly flammable and has a low flash point.

### 5. Calibration

Maintain a laboratory log of all calibrations.

**5.1 Probe Nozzle.** Probe nozzles shall be calibrated before their initial use in the field. Using a micrometer, measure the inside diameter of the nozzle to the nearest

0.02 mm (0.001 in.). Make three separate measurements using different diameters each time, and obtain the average of the measurements. The difference between the high and low numbers shall not exceed 0.1 mm (0.004 in.). When nozzles become nicked, dented, or corroded, they shall be reshaped, sharpened, and recalibrated before use. Each nozzle shall be permanently and uniquely identified.

**5.2 Pilot Tube.** The Type A pilot tube assembly shall be calibrated according to the procedure outlined in Section 4 of Method 2.

**5.3 Metering System.** Before its initial use in the field, the metering system shall be calibrated according to the procedure outlined in APTD-0578. Instead of physically adjusting the dry gas meter dial readings to correspond to the wet test meter readings, calibration factors may be used to mathematically correct the gas meter dial readings to the proper values. Before calibrating the metering system, it is suggested that a leak-check be conducted. For metering systems having diaphragm pumps, the normal leak-check procedure will not detect leaks within the pump. For these cases the following leak-check procedure is suggested: make a 10-minute calibration run at 0.00057 m<sup>3</sup>/min (0.02 cfm); at the end of the run, take the difference of the measured wet test meter run and dry gas meter volume; divide the difference by 10, and get the leak rate. The leak rate should not exceed 0.00057 m<sup>3</sup>/min (0.02 cfm).

After each field use, the calibration of the metering system shall be checked by performing three calibration runs at a single, intermediate orifice setting (based on runs at a single field test), with the vacuum set at the previous field test, during the test series. To maximum value reached during the wet test. To maximum value reached during the wet test. To maximum value reached during the wet test. To maximum value reached during the wet test.

Alternative procedures, e.g., using the orifice meter coefficients, may be used, subject to the approval of the Administrator.

**Note.**—If the dry gas meter coefficient values obtained before and after a test series differ by more than 5 percent, the test series shall either be voided, or calculations for the test series shall be performed using whichever meter coefficient value (i.e., before or after) gives the lower value of total sample volume.

**5.4 Probe Heater Calibration.** The probe heating value of total sample volume. This probe heating value shall be calibrated before its initial use in the system according to the procedure outlined in APTD-0578. Probes constructed according to APTD-0581 need not be calibrated if the calibration curves in APTD-0578 are used.

**5.5 Temperature Gauge.** Use the procedure in Section 4.3 of Method 2 to calibrate in-stack temperature gauges. Dual thermometers, such as are used for the dry gas meter and condenser outlet, shall be calibrated against mercury-in-glass thermometers.

**5.6 Leak Check of Metering System Shown in Figure 5-4.** That portion of the sampling train from the pump to the orifice meter should be leak checked prior to initial use and after each shipment. Leakage after the pump will result in less volume being recorded than is actually sampled. The following procedure is suggested (see Figure 5-4): Close the main valve on the meter box. Insert a one-hole rubber stopper with rubber tubing attached into the orifice exhaust pipe. Disconnect and attach the low side of the orifice manometer. Close off the vent the low side of the orifice manometer. Pressurize the system to 13 to 18 cm (5 to 7 in.) water column by blowing into the rubber tubing. Pinch off the tubing and observe the manometer for one minute. A loss of pressure on the manometer indicates a leak in the meter box; leaks, if present, must be corrected.

**5.7 Barometer.** Calibrate against a mercury barometer.

### 6. Calculations

Carry out calculations, retaining at least one extra decimal figure beyond that of the acquired data. Round off figures after the final calculation. Other forms of the equations may be used as long as they give equivalent results.

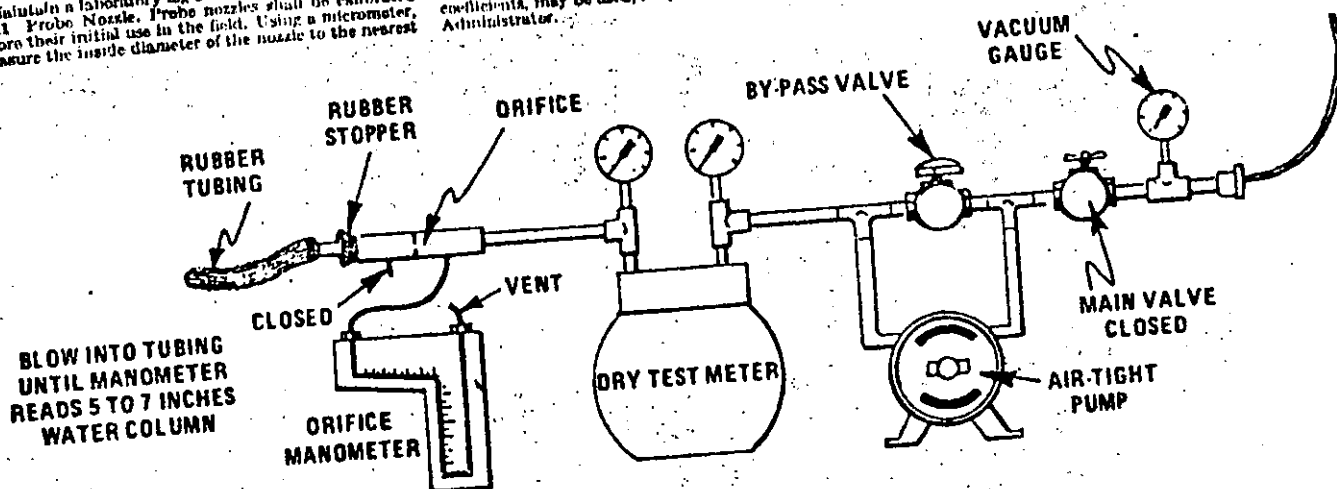


Figure 5-4. Leak check of meter box.

- 6.1 Nomenclature**
- $A_n$  = Cross-sectional area of nozzle, m<sup>2</sup> (ft<sup>2</sup>).
  - $B_m$  = Water vapor in the gas stream, proportion by volume.
  - $C$  = Acetone blank residue concentrations, mg/g.
  - $C_s$  = Concentration of particulate matter in stack gas, dry basis, corrected to standard conditions, g/dscm (g/dscf).
  - $I$  = Percent of isokinetic sampling.
  - $L$  = Maximum acceptable leakage rate for either a pre-test leak check or for a leak check following a component change, equal to 0.00057 m<sup>3</sup>/min (0.02 cfm) or 4 percent of the average sampling rate, whichever is less.
  - $L_d$  = Individual leakage rate observed during the leak check conducted prior to the "pre-test" component change (1, 2, 3, ..., n), m<sup>3</sup>/min (cfm).
  - $L_p$  = Leakage rate observed during the post-test leak check, m<sup>3</sup>/min (cfm).
  - $m$  = Total amount of particulate matter collected, mg.
  - $M_w$  = Molecular weight of water, 18.0 g/g-mole (18.0 lb/lb-mole).
  - $m_s$  = Mass of residue of acetone after evaporation, mg.
  - $P_{bar}$  = Barometric pressure at the sampling site, mm Hg (in. Hg).
  - $P_s$  = Absolute stack gas pressure, mm Hg (in. Hg).
  - $P_{std}$  = Standard absolute pressure, 760 mm Hg (29.92 in. Hg).

- $R$  = Ideal gas constant, 0.08206 m<sup>3</sup>-atm/g-mole-K (21.85 in. Hg-ft<sup>3</sup>/lb-mole-R).
- $T_m$  = Absolute average dry gas meter temperature (see Figure 5-2), °K (°F).
- $T_s$  = Absolute average stack gas temperature (see Figure 5-2), °K (°F).
- $T_{std}$  = Standard absolute temperature, 293° K (528° R).
- $V_s$  = Volume of acetone blank, ml.
- $V_{wv}$  = Volume of acetone used in wash, ml.
- $V_{wv}$  = Total volume of liquid collected in impingers and silica gel (see Figure 5-3), ml.
- $V_m$  = Volume of gas sample as measured by dry gas meter, dscm (dscf).
- $V_{std}$  = Volume of gas sample measured by the dry gas meter, corrected to standard conditions, dscm (dscf).
- $V_{std}(w)$  = Volume of water vapor in the gas sample, corrected to standard conditions, scm (scf).
- $V_s$  = Stack gas velocity, calculated by Method 2, Equation 2-9, using data obtained from Method 4, m/sec (ft/sec).
- $W_s$  = Weight of residue in acetone wash, mg.
- $Y$  = Dry gas meter calibration factor.
- $\Delta H$  = A vapor pressure differential across the orifice meter (see Figure 5-2), mm Hg (in. Hg).
- $\rho$  = Density of acetone, mg/ml (see label on bottle).
- $\rho_w$  = Density of water, 0.9982 g/ml (0.02201 lb/ml).
- $t$  = Total sampling time, min.

- $t_s$  = Sampling time interval, from the beginning of a run until the first component change, min.
- $t_{sc}$  = Sampling time interval, between two successive component changes, beginning with the interval between the first and second changes, min.
- $t_{sn}$  = Sampling time interval, from the final (nth) component change until the end of the sampling run, min.
- $\gamma$  = Specific gravity of mercury.
- $\%$  = Conversion to percent.

**6.2 Average dry gas meter temperature and average orifice pressure drop.** See data sheet (Figure 5-2).

**6.3 Dry (gas) Volume.** Correct the sample volume measured by the dry gas meter to standard conditions (20° C, 760 mm Hg or 68° F, 29.92 in. Hg) by using Equation 5-1.

$$V_{m(std)} = V_m Y \left( \frac{T_{std}}{T_m} \right) \left[ \frac{P_{bar} + \frac{\Delta H}{13.6}}{P_{std}} \right]$$

$$= K_1 V_m Y \frac{P_{bar} + (\Delta H/13.6)}{T_m}$$

Equation 5-1

where:  
 $m = 0.39 \times 10^{-3} \text{ K/mm Hg for metric units}$   
 $= 1.64 \times 10^{-3} \text{ in. Hg for English units}$

Note.—Equation 5-1 can be used as written unless the leakage rate observed during any of the mandatory leak checks (4.4.1), the post-test leak check or leak checks conducted prior to component changes exceeds  $L_0$ . If  $L_0$  or  $L_1$  exceeds  $L_0$ , Equation 5-1 must be modified as follows:

(a) Case I. No component changes made during sampling run. In this case, replace  $L_0$  in Equation 5-1 with the expression:

$$V_m = (L_0 - I_0)\theta$$

(b) Case II. One or more component changes made during the sampling run. In this case, replace  $V_m$  in Equation 5-1 by the expression:

$$\left[ V_m - (L_1 - I_0)\theta_1 - \sum_{i=2}^n (L_i - I_{i-1})\theta_i - (L_n - I_n)\theta_n \right]$$

and substitute only for those leakage rates ( $L_0$  or  $L_1$ ) which exceed  $L_0$ .

#### 6.4 Volume of water vapor.

Equation 5-2

$$V_w(\text{std}) = V_{12} \left( \frac{P_w}{P_{\text{std}}} \right) \left( \frac{RT_{\text{std}}}{P_{\text{std}}} \right) = K_2 V_{12}$$

where:  
 $K_2 = 0.00133 \text{ m}^3/\text{mol for metric units}$   
 $= 0.04707 \text{ ft}^3/\text{mol for English units}$   
 6.5 Moisture Content.

$$B_{wv} = \frac{V_w(\text{std})}{V_m(\text{std}) + V_w(\text{std})}$$

Equation 5-3

$$I = \frac{100 T_0 [K_2 V_{12} + (V_m/T_0) (P_{\text{std}} + \Delta H/13.6)]}{60 \theta_0 P_0 A_n}$$

Equation 5-7

where:  
 $K_1 = 0.00344 \text{ mm Hg} \cdot \text{m}^3/\text{mol} \cdot ^\circ\text{K for metric units}$   
 $= 0.02669 \text{ in. Hg} \cdot \text{ft}^3/\text{mol} \cdot ^\circ\text{R for English units}$   
 6.11.2 Calculation From Intermediate Values.

$$I = \frac{T_0 V_m(\text{std}) P_{\text{std}} 100}{T_{\text{std}} V_{12} \theta A_n P_0 60 (1 - B_{wv})}$$

$$= K_1 \frac{T_0 V_m(\text{std})}{P_0 V_{12} \theta A_n (1 - B_{wv})}$$

Equation 5-8

where:  
 $K_1 = 4.320 \text{ for metric units}$   
 $= 0.02450 \text{ for English units}$

6.12 Acceptable Results. If 90 percent  $\leq I \leq 110$  percent, the results are acceptable. If the results are low in comparison to the standard and  $I$  is beyond the acceptable range, or if  $I$  is less than 90 percent, the Administrator may opt to accept the results. Use Citation 4 to make judgments. Otherwise, reject the results and repeat the test.

#### 7. Bibliography.

1. Addendum to Specifications for Incinerator Testing at Federal Facilities, PHS, NCAPC, Dec. 6, 1967.
2. Martin, Robert M. Construction Details of Isokinetic Source-Sampling Equipment, Environmental Protection Agency, Research Triangle Park, N.C., APTD-66-1, April, 1971.
3. Kohn, Jerome J. Maintenance, Calibration, and Operation of Isokinetic Source Sampling Equipment, Environmental Protection Agency, Research Triangle Park, N.C., APTD-66-6, March, 1972.
4. Smith, W. R., R. T. Shuchman, and W. F. Todd. A Method of Interpreting Stack Sampling Data. Paper Presented at the 6th Annual Meeting of the Air Pollution Control Association, St. Louis, Mo. June 14-19, 1970.
5. Smith, W. R., et al. Stack Gas Sampling Improved and Simplified With New Equipment. AFCA Paper No. 67-119, 1967.
6. Specifications for Incinerator Testing at Federal Facilities, PHS, NCAPC, 1967.
7. Shuchman, R. T. Adjustments in the EPA Normograph for Different Total Tube Coefficients and Dry Molecular Weights. Stack Sampling News 2:4-11, October, 1974.

Note.—In saturated or water droplet laden gas streams, two calculations of the moisture content of the gas are possible, one from the impinger analysis (Equation 5-3), and a second from the assumption of saturated conditions. The lower of the two values of  $B_{wv}$  shall be considered correct. The procedure for determining the moisture content based upon assumption of saturated conditions is given in the Note of Section 1.2 of Method 4. For the purposes of this method, the average stack gas temperature from Figure 5-2 may be used to make this determination, provided that the accuracy of the in-stack temperature sensor is  $\pm 1^\circ\text{C}$  ( $2^\circ\text{F}$ ).

#### 6.6 Acetone Blank Concentration.

$$C_a = \frac{m_{a0}}{V_{a0} P_a}$$

Equation 5-4

#### 6.7 Acetone Wash Blank.

$$W_a = C_a V_{a0} P_a$$

Equation 5-5

6.8 Total Particulate Weight. Determine the total particulate catch from the sum of the weights obtained from containers 1 and 2 less the acetone blank (see Figure 5-3). Note.—Refer to Section 4.1.5 to assist in calculation of results involving two or more filter assemblies or two or more sampling trains.

#### 6.9 Particulate Concentration.

$$C_p = (0.001 \text{ g/mg}) (m_p/V_m(\text{std}))$$

Equation 5-6

#### 6.10 Conversion Factors.

| From            | To               | Multiply by              |
|-----------------|------------------|--------------------------|
| cf              | m <sup>3</sup>   | 0.02832                  |
| ft <sup>3</sup> | m <sup>3</sup>   | 15.45                    |
| ft <sup>3</sup> | liters           | 2.832 × 10 <sup>-2</sup> |
| ft <sup>3</sup> | g m <sup>3</sup> | 25.31                    |

#### 6.11 Isokinetic Variation.

##### 6.11.1 Calculation From Raw Data.

8. Vollaro, R. F. A Survey of Commercially Available Instrumentation for the Measurement of Low-Range Gas Velocities. U.S. Environmental Protection Agency, Emission Measurement Branch, Research Triangle Park, N.C. November, 1976 (unpublished paper).

9. Annual Book of ASTM Standards, Part 28, Gaseous Fuels; Coal and Coke; Atmospheric Analysis. American Society for Testing and Materials, Philadelphia, Pa. 1974, pp. 617-622.

#### METHOD 6—DETERMINATION OF SULFUR DIOXIDE EMISSIONS FROM STATIONARY SOURCES

##### 1. Principle and Applicability

1.1 Principle. A gas sample is extracted from the sampling point in the stack. The sulfuric acid mist (including sulfur trioxide) and the sulfur dioxide are separated. The sulfur dioxide fraction is measured by the bariumthionitrate titration method.

1.2 Applicability. This method is applicable for the determination of sulfur dioxide emissions from stationary sources. The minimum detectable limit of the method has been determined to be 3.4 milligrams (mg) of  $\text{SO}_2/\text{m}^3$  ( $1.2 \times 10^{-2}$  lb/ft<sup>3</sup>). Although no upper limit has been established, tests have shown that concentrations as high as 80,000 mg/m<sup>3</sup> of  $\text{SO}_2$  can be collected efficiently in two budget impingers, each containing 15 milliliters of 3 percent hydrogen peroxide, at a rate of 1.0 lpm for 20 minutes. Based on theoretical calculations, the upper concentration limit in a 25-liter sample is about 93,300 mg/m<sup>3</sup>.

Possible interferences are free ammonia, water-soluble cations, and fluorides. The cations and fluorides are removed by glass wool filters and an isopropanol bubbler, and hence do not affect the  $\text{SO}_2$  analysis. When samples are being taken from a gas stream with high concentrations of very fine metallic fumes (such as in bulk to control devices), a methacrylate glass fiber filter must be used in place of the glass wool plug, i.e., the one in the probe to remove the carbon interferences.

Free ammonia interferes by reacting with  $\text{SO}_2$  to form particulate sulfite and by reacting with the indicator. If free ammonia is present (this can be determined by knowledge of the process and noting white particulate matter in the probe and isopropanol bubbler), alternative methods, subject to the approval of the Administrator, U.S. Environmental Protection Agency, are required.

##### 2. Apparatus

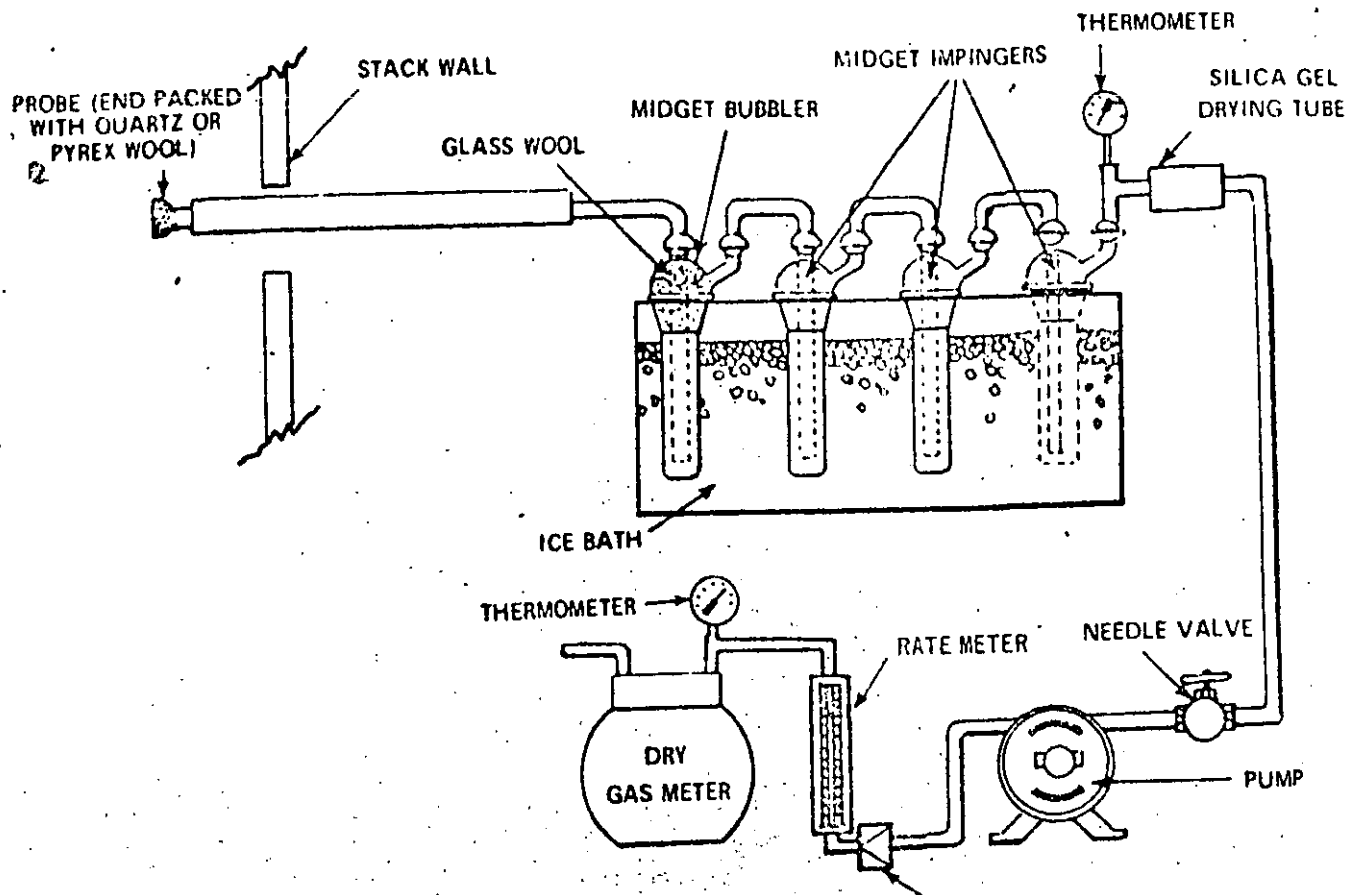


Figure 6-1. SO<sub>2</sub> sampling train.

**2.1 Sampling.** The sampling train is shown in Figure 6-1, and component parts are discussed below. The tester has the option of substituting sampling equipment described in Method 8 in place of the midget impinger equipment of Method 6. However, the Method 8 train must be modified to include a heated filter between the probe and isopropanol impinger, and the operation of the sampling train and sample analysis must be at the flow rates and solution volumes defined in Method 8.

The tester also has the option of determining SO<sub>2</sub> simultaneously with particulate matter and moisture determinations by (1) replacing the water in a Method 8 impinger system with 3 percent peroxide solution, or (2) by replacing the Method 8 water impinger system with a Method 8 isopropanol-filter-peroxide system. The analysis for SO<sub>2</sub> must be consistent with the procedure in Method 8.

**2.1.1 Probe.** Borosilicate glass, or stainless steel (other materials of construction may be used, subject to the approval of the Administrator), approximately 6-mm inside diameter, with a heating system to prevent water condensation and a filter (either in-stack or heated out-stack) to remove particulate matter, including sulfuric acid mist. A plug of glass wool is a satisfactory filter.

**2.1.2 Bubbler and Impingers.** One midget bubbler, with medium-coarse glass frit and borosilicate or quartz glass wool packed in top (see Figure 6-1) to prevent sulfuric acid mist carryover, and three 30-ml midget impingers. The bubbler and midget impingers must be connected in series with leak-free glass connectors. Silicone grease may be used, if necessary, to prevent leakage. At the option of the tester, a midget impinger may be used in place of the midget bubbler.

Other collection absorbers and flow rates may be used, but are subject to the approval of the Administrator. Also, collection efficiency must be shown to be at least 99 percent for each test run and must be documented after the report. If the efficiency is found to be acceptable after a series of three tests, further documentation is not required. To conduct the efficiency test, an extra absorber must be added and analyzed separately. This extra absorber must not contain more than 1 percent of the total SO<sub>2</sub>.

**2.1.3 Glass Wool.** Borosilicate or quartz.

**2.1.4 Stop-cock (Grease).** Acetone-insoluble, heat-stable silicone grease may be used, if necessary.

**2.1.5 Temperature Gauge.** Dial thermometer, or equivalent, to measure temperature of gas leaving impinger train to within 1° C (2° F).

**2.1.6 Drying Tube.** Tube packed with 6- to 16-mesh indicating type silica gel, or equivalent, to dry the gas

sample and to protect the meter and pump. If the silica gel has been used previously, dry at 175° C (350° F) for 2 hours. New silica gel may be used as received. Alternatively, other types of desiccants (equivalent or better) may be used, subject to approval of the Administrator.

**2.1.7 Valve.** Needle valve, to regulate sample gas flow rate.

**2.1.8 Pump.** Leak-free diaphragm pump, or equivalent, to pull gas through the train. Install a small tank between the pump and rate meter to eliminate the pulsation effect of the diaphragm pump on the rotameter.

**2.1.9 Rate Meter.** Rotameter, or equivalent, capable of measuring flow rate to within 2 percent of the selected flow rate of about 1000 cc/min.

**2.1.10 Volume Meter.** Dry gas meter, sufficiently accurate to measure the sample volume within 2 percent, calibrated at the selected flow rate and conditions actually encountered during sampling, and equipped with a temperature gauge (dial thermometer, or equivalent) capable of measuring temperature to within 3° C (5.4° F).

**2.1.11 Barometer.** Mercury, aneroid, or other barometer capable of measuring atmospheric pressure to within 2.5 mm Hg (0.1 in. Hg). In many cases, the barometric reading may be obtained from a nearby national weather service station, in which case the station value (which is the absolute barometric pressure) shall be requested and an adjustment for elevation differences between the weather station and sampling point shall be applied at a rate of minus 2.5 mm Hg (0.1 in. Hg) per 30 m (100 ft) elevation increase or vice versa for elevation decrease.

**2.1.12 Vacuum Gauge.** At least 760 mm Hg (30 in. Hg) gauge, to be used for leak check of the sampling train.

**2.2 Sample Recovery.**

**2.2.1 Wash bottles.** Polyethylene or glass, 500 ml, two.

**2.2.2 Storage Bottles.** Polyethylene, 100 ml, to store impinger samples (one per sample).

**2.3 Analysis.**

**2.3.1 Pipettes.** Volumetric type, 5-ml, 20-ml (one per sample), and 25-ml sizes.

**2.3.2 Volumetric Flasks.** 100-ml size (one per sample) and 100-ml size.

**2.3.3 Burettes.** 5- and 50-ml sizes.

**2.3.4 Erlenmeyer Flasks.** 250-ml size (one for each sample, blank, and standard).

**2.3.5 Dropping Bottle.** 125-ml size, to add indicator.

**2.3.6 Graduated Cylinder.** 100-ml size.

**2.3.7 Spectrophotometer.** To measure absorbance at 352 nanometers.

### 3. Reagents

Unless otherwise indicated, all reagents must conform to the specifications established by the Committee on Analytical Reagents of the American Chemical Society. Where such specifications are not available, use the best available grade.

#### 3.1 Sampling.

**3.1.1 Water.** Deionized, distilled to conform to ASTM specification D1193-71, Type 3. At the option of the analyst, the K<sub>2</sub>Cr<sub>2</sub>O<sub>7</sub> test for oxidizable organic matter may be omitted when high concentrations of organic matter are not expected to be present.

**3.1.2 Isopropanol, 80 percent.** Mix 80 ml of isopropanol with 20 ml of deionized, distilled water. Check each lot of isopropanol for peroxide impurities as follows: shake 10 ml of isopropanol with 10 ml of freshly prepared 10 percent potassium iodide solution. Prepare a blank by similarly treating 10 ml of distilled water. After 1 minute, read the absorbance at 252 nanometers on a spectrophotometer. If absorbance exceeds 0.1, reject alcohol for use.

Peroxides may be removed from isopropanol by redistilling or by passage through a column of activated alumina; however, reagent grade isopropanol with suitably low peroxide levels may be obtained from commercial sources. Rejection of contaminated lots may, therefore, be a more efficient procedure.

**3.1.3 Hydrogen Peroxide, 3 Percent.** Dilute 30 percent hydrogen peroxide 1:9 (v/v) with deionized, distilled water (30 ml is needed per sample). Prepare fresh daily.

**3.1.4 Potassium Iodide Solution, 10 Percent.** Dissolve 10.0 grams KI in deionized, distilled water and dilute to 100 ml. Prepare when needed.

#### 3.2 Sample Recovery.

**3.2.1 Water.** Deionized, distilled, as in 3.1.1.

**3.2.2 Isopropanol, 80 Percent.** Mix 80 ml of isopropanol with 20 ml of deionized, distilled water.

#### 3.3 Analysis.

**3.3.1 Water.** Deionized, distilled, as in 3.1.1.

**3.3.2 Isopropanol, 80 percent.**

**3.3.3 Thion Indicator.** 1-(4-arsenophenyl)-2-naphthol-3,6-disulfonic acid, disodium salt, or equivalent. Dissolve 0.20 g in 100 ml of deionized, distilled water.

**3.3.4 Barium Perochlorate Solution, 0.005 N.** Dissolve 1.05 g of barium perchlorate trihydrate [Ba(ClO<sub>4</sub>)<sub>3</sub>·3H<sub>2</sub>O] in 200 ml distilled water and dilute to 1 liter with isopropanol. Alternatively, 1.72 g of [BaCl<sub>2</sub>·2H<sub>2</sub>O] may be used instead of the perchlorate standard as in Section 8.8.

3.5. Sulfuric Acid Standard, 0.0100 N. Purchase or standardize to 0.0100 N against 0.0100 N NaOH which has previously been standardized against potassium acid phthalate (primary standard grade).

#### 4. Procedure

##### 4.1. Sampling

4.1.1. Preparation of collection train. Measure 15 ml of 80 percent isopropanol into the midjet bubbler and 15 ml of 3 percent hydrogen peroxide into each of the first two midjet impingers. Leave the final midjet impinger dry. Assemble the train as shown in Figure 6-1. Adjust probe heater to a temperature sufficient to prevent water condensation. Place crushed ice and water around the impingers.

4.1.2. Leak-check procedure. A leak check prior to the sampling run is optional; however, a leak check after the sampling run is mandatory. The leak-check procedure is as follows:

With the probe disconnected, place a vacuum gauge at the inlet to the bubbler and pull a vacuum of 20 mm (10 in.) Hg; plug or pinch off the outlet of the flow meter, and then turn off the pump. The vacuum shall remain stable for at least 30 seconds. Carefully release the vacuum gauge before releasing the flow meter end to prevent back flow of the impinger fluid.

Other leak check procedures may be used, subject to the approval of the Administrator, U.S. Environmental Protection Agency. The procedure used in Method 5 is not suitable for diaphragm pumps.

4.1.3. Sample collection. Record the initial dry gas meter reading and barometric pressure. To begin sampling, position the tip of the probe at the sampling point, connect the probe to the bubbler, and start the pump. Adjust the sample flow to a constant rate of approximately 1.0 liter/min as indicated by the rotameter. Maintain this constant rate ( $\pm 10$  percent) during the entire sampling run. Take readings (dry gas meter, temperatures at dry gas meter and at impinger outlet and rate meter) at least every 5 minutes. Add more ice during the run to keep the temperature of the gases leaving the last impinger at 20° C (68° F) or less. At the conclusion of each run, turn off the pump, remove probe from the stack, and record the final readings. Conduct a leak check as in Section 4.1.2. (This leak check is mandatory.) If a leak is found, void the test run. Drain the ice bath, and purge the remaining part of the train by drawing clean ambient air through the system for 15 minutes at the sampling rate.

Clean ambient air can be provided by passing air through a charcoal filter or through an extra midjet impinger with 15 ml of 3 percent  $\text{H}_2\text{O}_2$ . The tester may opt to simply use ambient air, without purification.

4.2. Sample recovery. Disconnect the impingers after purging. Discard the contents of the midjet bubbler. Pour the contents of the midjet impingers into a leak-free polyethylene bottle for shipment. Rinse the three midjet impingers and the connecting tubes with deionized, distilled water, and add the washings to the same storage container. Mark the fluid level. Seal and identify the sample container.

4.3. Sample Analysis. Note level of liquid in container, and confirm whether any sample was lost during shipment; note this on analytical data sheet. If a noticeable amount of leakage has occurred, either void the sample or use methods, subject to the approval of the Administrator, to correct the final results.

Transfer the contents of the storage container to a 100-ml volumetric flask and dilute to exactly 100 ml with deionized, distilled water. Pipette a 20-ml aliquot of this solution into a 250-ml Erlenmeyer flask, add 80 ml of 100 percent isopropanol and two to four drops of thion indicator, and titrate to a pink endpoint using 0.0100 N barium perchlorate. Repeat and average the titration volumes. Run a blank with each series of samples. Replicate titrations must agree within 1 percent or 0.2 ml, whichever is larger.

(Note.—Protect the 0.0100 N barium perchlorate solution from evaporation at all times.)

#### 5. Calibration

##### 5.1. Metering System

5.1.1. Initial Calibration. Before its initial use in the field, first leak check the metering system (drying tube, needle valve, pump, rotameter, and dry gas meter) as

follows: place a vacuum gauge at the inlet to the drying tube and pull a vacuum of 20 mm (10 in.) Hg; plug or pinch off the outlet of the flow meter, and then turn off the pump. The vacuum shall remain stable for at least 30 seconds. Carefully release the vacuum gauge before releasing the flow meter end.

Next, calibrate the metering system (at the sampling flow rate specified by the method) as follows: connect an appropriately sized wet test meter (e.g., 1 liter per revolution) to the inlet of the drying tube. Make three independent calibration runs, using at least five revolutions of the dry gas meter per run. Calculate the calibration factor,  $Y$  (wet test meter calibration volume divided by the dry gas meter volume, both volumes adjusted to the same reference temperature and pressure), for each run, and average the results. If any  $Y$  value deviates by more than 2 percent from the average, the metering system is unacceptable for use. Otherwise, use the average as the calibration factor for subsequent test runs.

5.1.2. Post-Test Calibration Check. After each field test series, conduct a calibration check as in Section 5.1.1 above, except for the following variations: (a) the leak check is not to be conducted, (b) three, or more revolutions of the dry gas meter may be used, and (c) only two independent runs need be made. If the calibration factor does not deviate by more than 5 percent from the initial calibration factor (determined in Section 5.1.1), then the dry gas meter volumes obtained during the test series are acceptable. If the calibration factor deviates by more than 5 percent, recalibrate the metering system as in Section 5.1.1, and for the calculations, use the calibration factor (initial or recalibration) that yields the lower gas volume for each test run.

5.2. Thermometers. Calibrate against mercury-in-glass thermometers.

5.3. Rotameter. The rotameter need not be calibrated but should be cleaned and maintained according to the manufacturer's instruction.

5.4. Barometer. Calibrate against a mercury barometer.

5.5. Barium Perchlorate Solution. Standardize the barium perchlorate solution against 25 ml of standard sulfuric acid to which 100 ml of 100 percent isopropanol has been added.

#### 6. Calculations

Carry out calculations, retaining at least one extra decimal figure beyond that of the acquired data. Round off figures after final calculation.

##### 6.1. Nomenclature

- $C_m$  = Concentration of sulfur dioxide, dry basis corrected to standard conditions, mg/dscm (lb/dscf).
- $N$  = Normality of barium perchlorate titrant, milliequivalents/ml.
- $P_{bar}$  = Barometric pressure at the exit orifice of the dry gas meter, mm Hg (in. Hg).
- $P_{std}$  = Standard absolute pressure, 760 mm Hg (21.92 in. Hg).
- $T_m$  = Average dry gas meter absolute temperature, °K (°F).
- $T_{std}$  = Standard absolute temperature, 293° K (69° F).
- $V_m$  = Volume of sample aliquot titrated, ml.
- $V_m$  = Dry gas volume as measured by the dry gas meter, dcm (def).
- $V_{m(Std)}$  = Dry gas volume measured by the dry gas meter, corrected to standard conditions, dscm (dscf).
- $V_{std}$  = Total volume of solution in which the sulfur dioxide sample is contained, 100 ml.
- $V_t$  = Volume of barium perchlorate titrant used for the sample, ml (average of replicate titrations).
- $V_{t0}$  = Volume of barium perchlorate titrant used for the blank, ml.
- $Y$  = Dry gas meter calibration factor.
- 32.03 = Equivalent weight of sulfur dioxide.

6.2. Dry sample gas volume, corrected to standard conditions.

$$V_{m(Std)} = V_m Y \left( \frac{T_{std}}{T_m} \right) \left( \frac{P_{bar}}{P_{std}} \right) = K_1 Y \frac{V_m P_{bar}}{T_m}$$

Equation 6-1

where:

- $K_1 = 0.858 \text{ } ^\circ\text{K/mm Hg}$  for metric units,
- $= 17.63 \text{ } ^\circ\text{F/in. Hg}$  for English units,
- 6.3. Sulfur dioxide concentration,

$$C_{SO_2} = K_2 \frac{(V_t - V_{t0}) N \left( \frac{V_{std}}{V_m} \right)}{V_{m(Std)}}$$

Equation 6-2

where:

- $K_2 = 32.03 \text{ mg/meq}$  for metric units,
- $= 7.06 \times 10^{-3} \text{ lb/meq}$  for English units.

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#### METHOD 7—DETERMINATION OF NITROGEN OXIDE EMISSIONS FROM STATIONARY SOURCES

##### 1. Principle and Applicability

1.1. Principle. A grab sample is collected in an evacuated flask containing a dilute sulfuric acid-hydrogen peroxide absorbing solution, and the nitrogen oxides, except nitrous oxide, are measured colorimetrically using the phenoldisulfonic acid (PDS) procedure.

1.2. Applicability. This method is applicable to the measurement of nitrogen oxides emitted from stationary sources. The range of the method has been determined to be 2 to 400 milligrams  $\text{NO}_x$  (as  $\text{NO}_2$ ) per dry standard cubic meter, without having to dilute the sample.

##### 2. Apparatus

2.1. Sampling (see Figure 7-1). Other grab sampling systems or equipment, capable of measuring sample volume to within  $\pm 2.0$  percent and collecting a sufficient sample volume to allow analytical reproducibility to within  $\pm 5$  percent, will be considered acceptable alternatives, subject to approval of the Administrator, U.S. Environmental Protection Agency. The following equipment is used in sampling:

2.1.1. Probe. Borosilicate glass tubing, sufficiently heated to prevent water condensation and equipped with an in-stack or out-stack filter to remove particulate matter (a plug of glass wool is satisfactory for this purpose). Stainless steel or Teflon tubing may also be used for the probe. Heating is not necessary if the probe remains dry during the purging period.

\* Mention of trade names or specific products does not constitute endorsement by the Environmental Protection Agency.

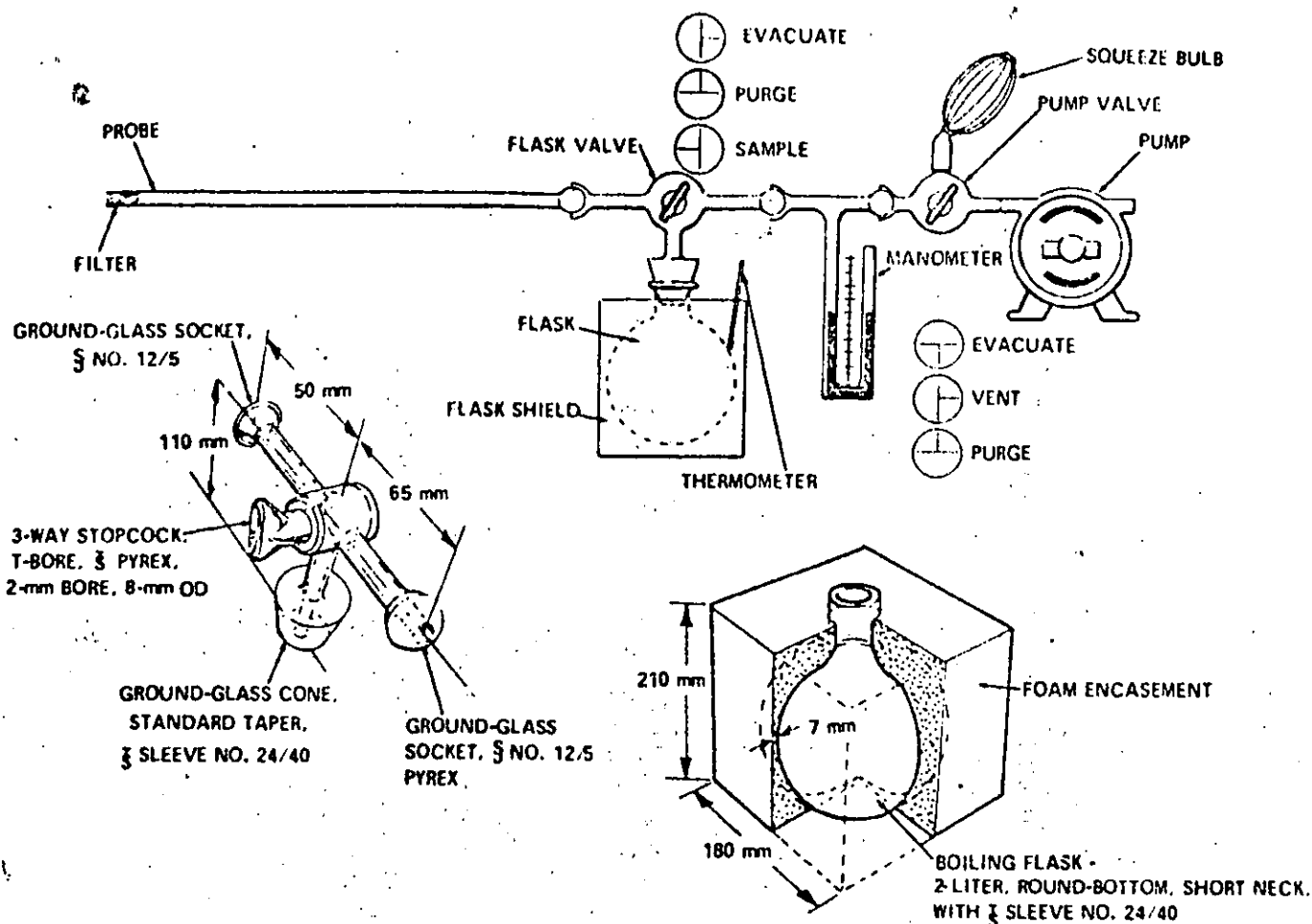


Figure 7-1. Sampling train, flask valve, and flask.

2.1.2 Collection Flask. Two-liter borosilicate, round bottom flask, with short neck and 2140 standard taper opening, protected against implosion or breakage.

2.1.3 Flask Valve. T-bore stopcock connected to a 24/40 standard taper joint.

2.1.4 Temperature Gauge. Dual-type thermometer, or other temperature gauge, capable of measuring 1° C (2° F) intervals from -5 to 50° C (23 to 123° F).

2.1.5 Vacuum Line. Tubing capable of withstanding a vacuum of 75 mm Hg (3 in. Hg) absolute pressure, with T-connection and T-bore stopcock.

2.1.6 Vacuum Gauge. U-tube manometer, 1 meter (36 in.), with 1-mm (0.1-in.) divisions, or other gauge capable of measuring pressure to within ±2.5 mm Hg (0.10 in. Hg).

2.1.7 Pump. Capable of evacuating the collection flask to a pressure equal to or less than 75 mm Hg (3 in. Hg) absolute.

2.1.8 Squeeze Bulb. One-way.

2.1.9 Volumetric Pipette. 25 ml.

2.1.10 Stopcock and Ground Joint Grease. A high-vacuum, high-temperature chlorofluorocarbon grease is required. Halocarbon 200SS has been found to be effective.

2.1.11 Barometer. Mercury, aneroid, or other barometer capable of measuring atmospheric pressure to within 2.5 mm Hg (0.1 in. Hg). In many cases, the barometric reading may be obtained from a nearby national weather service station, in which case the station value (which is the absolute barometric pressure) shall be requested and an adjustment for elevation differences between the weather station and sampling point shall be applied at a rate of minus 2.5 mm Hg (0.1 in. Hg) per 100 ft (30 m) elevation increase, or vice versa for elevation decrease.

2.2 Sample Recovery. The following equipment is required for sample recovery:

2.2.1 Graduated Cylinder. 50 ml with 1-ml divisions.

2.2.2 Storage Containers. Leak-free polyethylene bottles.

2.2.3 Wash Bottle. Polyethylene or glass.

2.2.4 Glass Stirring Rod.

2.2.5 Test Paper for Indicating pH. To cover the pH range of 7 to 11.

2.3 Analysis. For the analysis, the following equipment is needed:

2.3.1 Volumetric Pipettes. Two 1 ml, two 2 ml, one 3 ml, one 4 ml, two 10 ml, and one 25 ml for each sample and standard.

2.3.2 Porcelain Evaporating Dishes. 175- to 250-ml capacity with lip for pouring, one for each sample and each standard. The Coors No. 5006 (shallow-form, 195 ml) has been found to be satisfactory. Alternatively, polymethyl pentene beakers (Nalgene No. 1903, 180 ml), or glass beakers (150 ml) may be used. When glass beakers are used, etching of the beakers may cause solid matter to be present in the analytical stem; the solids should be removed by filtration (see Section 4.3).

2.3.3 Steam Bath. Low-temperature ovens or thermostatically controlled hot plates kept below 70° C (160° F) are acceptable alternatives.

2.3.4 Dropping Pipette or Dropper. Three required.

2.3.5 Polyethylene Pottleman. One for each sample and each standard.

2.3.6 Graduated Cylinder. 100 ml with 1-ml divisions.

2.3.7 Volumetric Flasks. 50 ml (one for each sample), 100 ml (one for each sample and each standard), and one for the working standard.  $\text{KNO}_3$  solution, and 1000 ml (one).

2.3.8 Spectrophotometer. To measure absorbance at 410 nm.

2.3.9 Graduated Pipette. 10 ml with 0.1-ml divisions.

2.3.10 Test Paper for Indicating pH. To cover the pH range of 7 to 14.

2.3.11 Analytical Balance. To measure to within 0.1 mg.

### 3. Hazards

Unless otherwise indicated, it is intended that all reagents conform to the specifications established by the Committee on Analytical Reagents of the American Chemical Society, where such specifications are available; otherwise, use the best available grade.

3.1 Sampling. To prepare the absorbing solution, cautiously add 2.8 ml concentrated  $\text{H}_2\text{SO}_4$  to 1 liter of deionized, distilled water. Mix well and add 6 ml of 3 percent hydrogen peroxide, freshly prepared from 30 percent hydrogen peroxide solution. The absorbing solution should be used within 1 week of its preparation. Do not expose to extreme heat or direct sunlight.

3.2 Sample Recovery. Two reagents are required for sample recovery:

3.2.1 Sodium Hydroxide (1N). Dissolve 40 g NaOH in deionized, distilled water and dilute to 1 liter.

3.2.2 Water. Deionized, distilled to conform to ASTM specification D1230-71, Type 3. At the option of the

analyst, the  $\text{KMnO}_4$  test for oxidizable organic matter may be omitted when high concentrations of organic matter are not expected to be present.

3.2 Analysis. For the analysis, the following reagents are required:

3.3.1 Fuming Sulfuric Acid. 15 to 18 percent by weight free sulfur trioxide. HANDLE WITH CAUTION.

3.3.2 Phenol. White solid.

3.3.3 Sulfuric Acid. Concentrated, 95 percent minimum assay. HANDLE WITH CAUTION.

3.3.4 Potassium Nitrate. Dried at 105 to 110° C (220 to 230° F) for a minimum of 2 hours just prior to preparation of standard solution.

3.3.5 Standard  $\text{KNO}_3$  Solution. Dissolve exactly 2.185 g of dried potassium nitrate ( $\text{KNO}_3$ ) in deionized, distilled water and dilute to 1 liter with deionized, distilled water in a 1,000-ml volumetric flask.

3.3.6 Working Standard  $\text{KNO}_3$  Solution. Dilute 10 ml of the standard solution to 100 ml with deionized distilled water. One milliliter of the working standard solution is equivalent to 100  $\mu\text{g}$  nitrogen dioxide ( $\text{NO}_2$ ).

3.3.7 Water. Deionized, distilled as in Section 3.2.2.

3.3.8 Phenolsulfonic Acid Solution. Dissolve 2.5 g of pure white phenol in 150 ml concentrated sulfuric acid on a steam bath. Cool, add 75 ml fuming sulfuric acid, and heat at 100° C (212° F) for 2 hours. Store in a dark, stoppered bottle.

### 4. Procedures

#### 4.1 Sampling.

4.1.1 Pipette 25 ml of absorbing solution into a sample flask, retaining a sufficient quantity for use in preparing the calibration standards. Insert the flask valve stopper into the flask with the valve in the "purge" position. Assemble the sampling train as shown in Figure 7-1 and place the probe at the sampling point. Make sure that all fittings are tight and leak-free, and that all ground glass joints have been properly greased with a high-vacuum, high-temperature chlorofluorocarbon-based stopcock grease. Turn the flask valve and the pump valve to their "evacuate" positions. Evacuate the flask to 75 mm Hg (3 in. Hg) absolute pressure, or less. Evacuation to a pressure approaching the vapor pressure of water at the existing temperature is desirable. Turn the pump valve to its "vent" position and turn off the pump. Check for leakage by observing the manometer for any pressure fluctuation. (Any variation



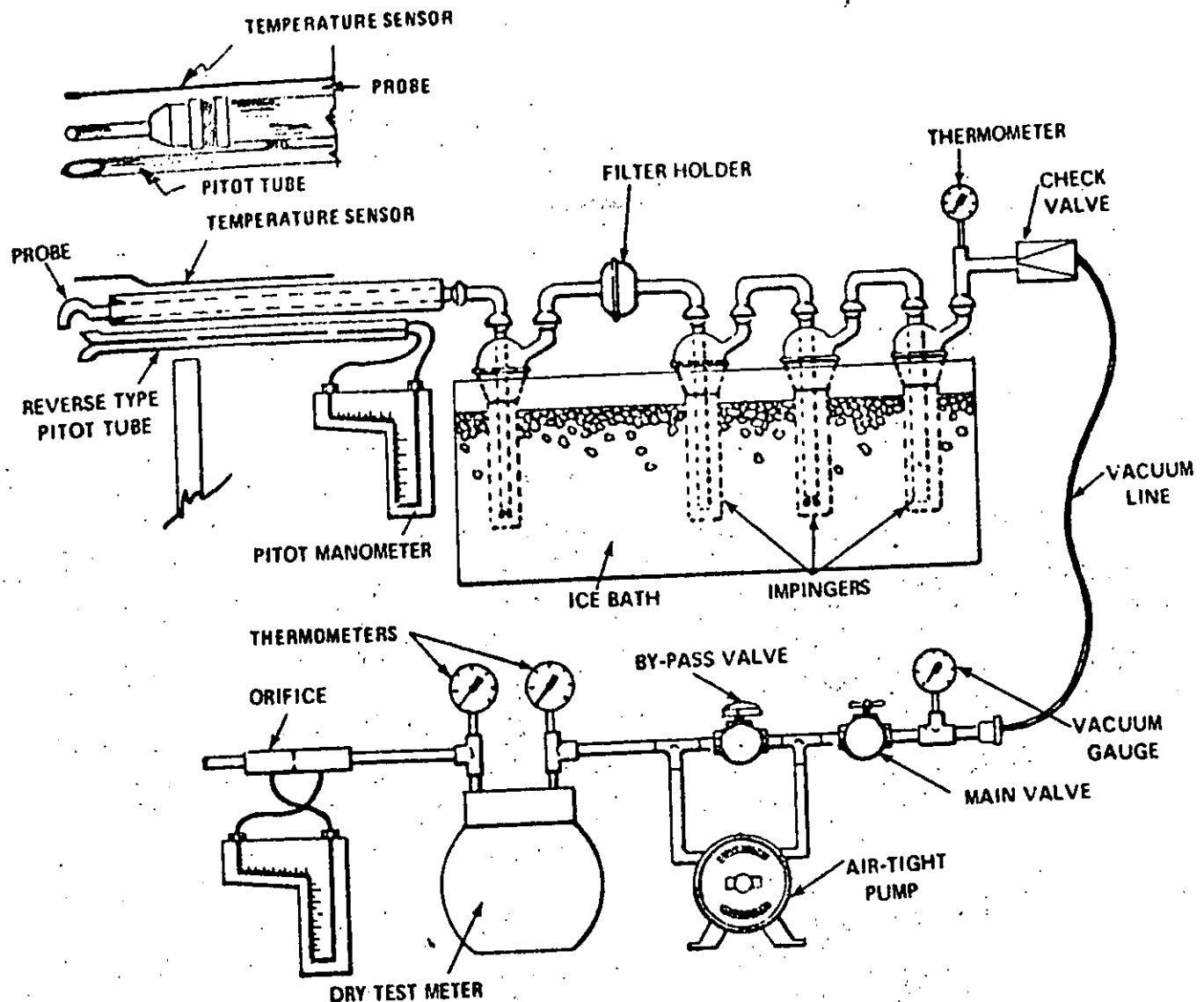


Figure 8-1. Sulfuric acid mist sampling train.

2.1.4 Differential Pressure Gauge. Same as Method 5, Section 2.1.4.

2.1.5 Filter Holder. Borosilicate glass, with a glass frit filter support and a silicone rubber gasket. Other gasket materials, e.g., Teflon or Viton, may be used subject to the approval of the Administrator. The holder design shall provide a positive seal against leakage from the outside or around the filter. The filter holder shall be placed between the first and second impingers. Note: Do not heat the filter holder.

2.1.6 Impingers—Four, as shown in Figure 8-1. The first and third shall be of the Greenburg-Smith design with standard tips. The second and fourth shall be of the Greenburg-Smith design, modified by replacing the insert with an approximately 13 millimeter (0.5 in.) ID glass tube, having an unobstructed tip located 13 mm (0.5 in.) from the bottom of the flask. Similar collection systems, which have been approved by the Administrator, may be used.

2.1.7 Metering System. Same as Method 5, Section 2.1.8.

2.1.8 Barometer. Same as Method 5, Section 2.1.9.

2.1.9 Gas Density Determination Equipment. Same as Method 5, Section 2.1.10.

2.1.10 Temperature Gauge, Thermometer, or equivalent, to measure the temperature of the gas leaving the impinger train to within 1°C (2°F).

2.2 Sample Recovery.

2.2.1 Wash Bottles. Polyethylene or glass, 500 ml. (two).

2.2.2 Graduated Cylinders, 250 ml, 1 liter. (Volume metric flasks may also be used.)

2.2.3 Storage Bottles. Leak-free polyethylene bottles, 100 ml size (two for each sampling run).

2.2.4 Trip Balance, 500-gram capacity, to measure to  $\pm 0.5$  g (necessary only if a moisture content analysis is to be done).

2.3 Analysis.

2.3.1 Pipettes. Volumetric 25 ml, 100 ml.

2.3.2 Burette, 50 ml.

2.3.3 Erlenmeyer Flask, 250 ml. (one for each sample blank and standard).

2.3.4 Graduated Cylinder, 100 ml.

2.3.5 Trip Balance, 500 g capacity, to measure to  $\pm 0.5$  g.

2.3.6 Dropping Bottle. To add indicator solution, 125-ml size.

### 3. Reagents

Unless otherwise indicated, all reagents are to conform to the specifications established by the Committee on Analytical Reagents of the American Chemical Society, where such specifications are available. Otherwise, use the best available grade.

#### 3.1 Sampling.

3.1.1 Filters. Same as Method 5, Section 3.1.1.

3.1.2 Silica Gel. Same as Method 5, Section 3.1.2.

3.1.3 Water. Deionized, distilled to conform to ASTM specification D1193-74, Type 3. At the option of the analyst, the KMnO<sub>4</sub> test for oxidizable organic matter may be omitted when high concentrations of organic matter are not expected to be present.

3.1.4 Isopropanol, 80 Percent. Mix 800 ml of isopropanol with 200 ml of deionized, distilled water.

Note.—Experience has shown that only A.C.S. grade isopropanol is satisfactory. Tests have shown that isopropanol obtained from commercial sources occasionally has peroxide impurities that will cause ex-

cessively high sulfuric acid mist measurement. Use the following test for detecting peroxides in each lot of isopropanol: Shake 10 ml of the isopropanol with 10 ml of freshly prepared 10 percent potassium iodide solution. Prepare a blank by similarly treating 10 ml of distilled water. After 1 minute, read the absorbance on a spectrophotometer at 352 nanometers. If the absorbance exceeds 0.1, the isopropanol shall not be used. Peroxides may be removed from isopropanol by redistilling, or by passage through a column of activated alumina. However, reagent-grade isopropanol with suitably low peroxide levels is readily available from commercial sources; therefore, rejection of contaminated lots may be more efficient than following the peroxide removal procedure.

3.1.5 Hydrogen Peroxide, 3 Percent. Dilute 100 ml of 30 percent hydrogen peroxide to 1 liter with deionized, distilled water. Prepare fresh daily.

3.1.6 Crushed Ice.

3.2 Sample Recovery.

3.2.1 Water. Same as 3.1.3.

3.2.2 Isopropanol, 80 Percent. Same as 3.1.4.

3.3 Analysis.

3.3.1 Water. Same as 3.1.3.

3.3.2 Isopropanol, 100 Percent.

3.3.3 Thorin Indicator, 1-(6-arsomphenylazo)-2-naphthol-3, 6-disulfonic acid, disodium salt, or equivalent. Dissolve 0.20 g in 100 ml of deionized, distilled water.

3.3.4 Barium Perchlorate Dihydrate (BaCl<sub>2</sub>·10H<sub>2</sub>O). Dissolve 1.95 g of barium perchlorate dihydrate in 100 ml of deionized, distilled water, and dilute to 1 liter.

In 200 ml deionized, distilled water, and dilute to 1 liter with isopropanol; 1.22 g of barium chloride dihydrate (BaCl<sub>2</sub>·2H<sub>2</sub>O) may be used instead of the barium perchlorate. Standardize with sulfuric acid as in Section 5.2.

This solution must be protected against evaporation at all times.



3.3.5 Sulfuric Acid Standard (0.0100 N). Purchase or standardize to  $\pm 0.0002$  N against 0.0100 N NaOH that has previously been standardized against primary standard potassium acid phthalate.

4. *Sturdness*

**Forest Preparation.** Follow the procedure outlined in Method 8, Section 4.1; filters should be inspected, but need not be desiccated, weighed, or identified. If the effluent gas can be considered dry, i.e., moisture free, the filter need not be weighed.

4.1.2 Preliminary Determinations. Follow the procedure outlined in Method 5, Section 4.1.2.

4.1.3 The preparation of Collected Train. Follow the procedure outlined in Method 5, Section 4.1.2 (except for the second paragraph and other obviously inappropriate parts) and use Figure A-1 instead of Figure 5.1. Replace the second paragraph with: "Place 100 ml of 50 percent hypophosphorous in the first impinger, 100 ml of 5 percent hypophosphorous in both the second and third im-

placers; retain a portion of each reagent for use as a blank solution. Place about 200 g of silicagel in the fourth beaker.

**NOTE.**—If moisture content is to be determined by impinger analysis, weigh each of the first three impingers (plus absorbing solution) to the nearest 0.5 g and record these weights. The weight of the silicon g.3 (or silicon gel plus container) must also be determined to the nearest 0.5 g and recorded.

4.1.4 **Pretest Leak-Check Procedure.** Follow the basic procedure outlined in Method 3, Section 4.1.4.1, noting that the probe heater shall be adjusted to the minimum temperature required to prevent condensation, and also that **whenever such as " " "plugging the inlet to the filter holder " " " shall be replaced by, " " " plugging the inlet to the first impinger " " "** The pretest leak-check is optional.

4.1.5 Train Operation. Follow the basic procedures outlined in Method 5, Section 4.1.5, in conjunction with the following special instructions. Data shall be recorded

on a sheet similar to the one in Figure 8. The sampling rate shall not exceed 0.001 m/min (0.04 cm) during the run. Periodically during the test, observe the connecting line between the probe and test impinger for signs of condensation. If it does occur, adjust the probe heater setting upward to the minimum temperature required to prevent condensation. If component changes become necessary during a run, a leak-check shall be done immediately before each change, according to the procedure outlined in Section 4.1.4.2 of Method 5 (with appropriate modifications, as mentioned in Section 4.1.4 of this method); record all leak rates. If the leakage rate(s) exceed the specified rate, the tester shall either void the run or shall plan to correct the sample volume as outlined in Section 6.3 of Method 5. Immediately after component changes, leak-checks are optional. If these leak-checks are done, the procedure outlined in Section 4.1.4.1 of Method 5 (with appropriate modifications) shall be used.

PLANT \_\_\_\_\_  
LOCATION \_\_\_\_\_  
OPERATOR \_\_\_\_\_  
DATE \_\_\_\_\_  
RUN NO. \_\_\_\_\_  
SAMPLE BOX NO. \_\_\_\_\_  
METER BOX NO. \_\_\_\_\_  
METER  $\Delta H$  \_\_\_\_\_  
C FACTOR \_\_\_\_\_  
PITOT TUBE COEFFICIENT,  $C_p$  \_\_\_\_\_

STATIC PRESSURE, mm Hg (in. Hg) \_\_\_\_\_

AMBIENT TEMPERATURE \_\_\_\_\_

BAROMETRIC PRESSURE \_\_\_\_\_

ASSUMED MOISTURE, % \_\_\_\_\_

PROBE LENGTH, m (ft) \_\_\_\_\_

NOZZLE IDENTIFICATION NO. \_\_\_\_\_

AVERAGE CALIBRATED NOZZLE DIAMETER, cm (in.) \_\_\_\_\_

PROBE HEATER SETTING \_\_\_\_\_

LEAK RATE, m<sup>3</sup>/min, (cfm) \_\_\_\_\_

PROBE LINER MATERIAL \_\_\_\_\_

FILTER NO. \_\_\_\_\_

**SCHEMATIC OF STACK CROSS SECTION**

[illegible]

**Figure 8-2. Field data.**

After turning off the pump and recording the final readings at the conclusion of each run, remove the probe from the stack. Conduct a post-test (mandatory) leak-check as in Section 4.4.3 of Method 5 (with appropriate modification) and record the leak rate. If the post-test leakage rate exceeds the specified acceptable rate, the tester shall either correct the sample volume, as outlined in Section 6.3 of Method 5, or shall void the run.

Drain the ice bath and, with the probe disconnected, purge the remaining part of the train, by drawing clean ambient air through the system for 15 minutes at the average flow rate used for sampling.

NOTE.—Clean ambient air can be provided by passing air through a charcoal filter. At the option of the tester, ambient air (without cleaning) may be used.

4.1.6 Calculation of Percent Linkage. Follow the procedure outlined in Method 5, Section 4.1.6.

#### 4.2 Sample Recovery.

#### 4.2.1 Container No. 1. If a moisture content analysis

is to be done, weigh the first impinger plus contents to the nearest 0.5 g and record this weight.

Transfer the contents of the first impinger to a 250-ml graduated cylinder. Rinse the probe, first impinger, all connecting glassware before the filter, and the front half of the filter holder with 50 percent isopropanol. Add the rinse solution to the cylinder. Dilute to 250 ml with 50 percent isopropanol. Add the filter to the solution, mix, and transfer to the storage container. Protect the solution against evaporation. Mark the level of liquid on the container and identify the sample container.

4.3.2 Container No. 2. If a moisture content analysis is to be done, weigh the second and third impingers (plus contents) to the nearest 0.5 g and record these weights. Also, weigh the spent silica gel (or silica gel plus impinger) to the nearest 0.5 g.

Transfer the solutions from the second and third impingers to a 100-ml graduated cylinder. Rinse all connecting glassware (including back half of filter holder) between the filter and silica gel impinger with deionized,

distilled water, and add this rinse water to the cylinder. Dilute to a volume of 100 ml with deionized, distilled water. Transfer the solution to a storage container. Mark the level of liquid on the container. Seal and identify the sample container.

4.3. Analysis.

Note the level of liquid in containers 1 and 2, and confirm whether or not any sample was lost during shipment; note this on the analytical data sheet. If a noticeable amount of leakage has occurred, either void the sample or use methods, subject to the approval of the Administrator, to correct the final results.

4.3.1. *Container No. 1.* Shake the container holding the isopropanol solution and the filter. If the filter breaks up, allow the fragments to settle for a few minutes before removing a sample. Pipette a 10-mL aliquot of this solution into a 250-mL Erlenmeyer flask, add 2 to 4 drops of thion indicator, and titrate to a pink endpoint using 0.010 N lithium perchlorate. Repeat the titration with a second aliquot of sample and average the titration.



values. Replicate titrations must agree within 1 percent or 0.2 ml, whichever is greater.

4.3.2. Contain No. 2. Thoroughly mix the solution in the container holding the contents of the second and third impingers. Pipette a 10-ml aliquot of sample into a 250-ml Erlenmeyer flask. Add 10 ml of isopropanol, 2 to 4 drops of thion indicator, and titrate to a pink endpoint using 0.01N barium perchlorate. Repeat the titration with a second aliquot of sample and average the titration values. Replicate titrations must agree within 1 percent or 0.2 ml, whichever is greater.

4.3.3. Blanks. Prepare blanks by adding 2 to 4 drops of thion indicator to 100 ml of 80 percent isopropanol. Titrate the blanks in the same manner as the samples.

#### 5. Calibration

5.1. Calibrate equipment using the procedures specified in the following sections of Method 5: Section 5.3 (metering system); Section 5.5 (temperature gauges); Section 5.7 (barometer). Note that the recommended leak-check of the metering system, described in Section 5.6 of Method 5, also applies to this method.

5.2. Standardize the barium perchlorate solution with 25 ml of standard sulfuric acid, to which 100 ml of 100 percent isopropanol has been added.

#### 6. Calculations

Note.—Carry out calculations retaining at least one extra decimal figure beyond that of the acquired data. Round off figures after final calculation.

##### 6.1. Nomenclature

$A_n$ —Cross-sectional area of nozzle,  $m^2$  ( $ft^2$ ).  
 $B_{ws}$ —Water vapor in the gas stream, proportion by volume.

$CH_2SO_3$ —Sulfuric acid (including  $SO_3$ ) concentration, g/dscm ( $lb/dscf$ ).

$CSO_2$ —Sulfur dioxide concentration, g/dscm ( $lb/dscf$ ).

$I$ —Percent of isokinetic sampling.

$N$ —Normality of barium perchlorate titrant, g equivalents/liter.

$P_{bar}$ —Barometric pressure at the sampling site, mm Hg (in. Hg).

$P_s$ —Absolute stack gas pressure, mm Hg (in. Hg).

$P_{std}$ —Standard absolute pressure, 760 mm Hg (29.92 in. Hg).

$T_a$ —Average absolute dry gas meter temperature (see Figure 8-2),  $^{\circ}K$  ( $^{\circ}F$ ).

$T_s$ —Average absolute stack gas temperature (see Figure 8-2),  $^{\circ}K$  ( $^{\circ}F$ ).

$T_{std}$ —Standard absolute temperature, 273 $^{\circ}K$  (32 $^{\circ}F$ ).

$V_s$ —Volume of sample aliquot titrated, 100 ml for  $H_2SO_4$  and 10 ml for  $SO_3$ .

$V_L$ —Total volume of liquid collected in impingers and silica gel, ml.

$V_m$ —Volume of gas sample as measured by dry gas meter, dcm (dscf).

$V_m(Std)$ —Volume of gas sample measured by the dry gas meter corrected to standard conditions, dcm (dscf).

$v_a$ —Average stack gas velocity, calculated by Method 2, Equation 2-9, using data obtained from Method 5, m/sec (ft/sec).

$V_{soln}$ —Total volume of solution in which the sulfuric acid or sulfur dioxide sample is contained, 250 ml or 1,000 ml, respectively.

$V_t$ —Volume of barium perchlorate titrant used for the sample, ml.

$V_{bl}$ —Volume of barium perchlorate titrant used for the blank, ml.

$Y$ —Dry gas meter calibration factor.

$\Delta H$ —Average pressure drop across orifice meter, mm (in.)  $H_2O$ .

$t$ —Total sampling time, min.

13.6—Specific gravity of mercury, 60 $^{\circ}C$ /min.

100—Conversion to percent.

6.2. Average dry gas meter temperature and average orifice pressure drop. See data sheet (Figure 8-2).

6.3. Dry Gas Volume. Correct the sample volume measured by the dry gas meter to standard conditions (20 $^{\circ}C$  and 760 mm Hg or 68 $^{\circ}F$  and 29.92 in. Hg) by using Equation 8-1.

$$V_m(Std) = V_m Y \left( \frac{T_{std}}{T_m} \right) \frac{P_{bar} + \left( \frac{\Delta H}{13.6} \right)}{P_{std}} \\ = K_1 V_m Y \frac{P_{bar} + (\Delta H/13.6)}{T_m}$$

Equation 8-1

where:  
 $K_1 = 0.3558$   $^{\circ}K$ /mm Hg for metric units.  
 $= 17.61$   $^{\circ}F$ /in. Hg for English units.

Note.—If the leak rate observed during any mandatory leak-checks exceeds the specified acceptable rate, the tester shall either correct the value of  $V_m$  in Equation 8-1 (as described in Section 6.3 of Method 5), or shall invalidate the test run.

6.4. Volume of Water Vapor and Moisture Content. Calculate the volume of water vapor using Equation 5-2 of Method 5. The weight of water collected in the impingers and silica gel can be directly converted to milliliters (the specific gravity of water is 1 g/ml). Calculate the moisture content of the stack gas, using Equation 5-3 of Method 5. The "Note" in Section 5.5 of Method 5 also applies to this method. Note that if the effluent gas stream can be considered dry, the volume of water vapor and moisture content need not be calculated.

6.5. Sulfuric acid mist (including  $SO_3$ ) concentration.

$$CH_2SO_3 = K_2 \frac{N(V_t - V_{bl}) \left( \frac{V_{soln}}{V_s} \right)}{V_m(Std)}$$

Equation 8-2

where:  
 $K_2 = 0.04904$  g/milliequivalent for metric units.  
 $= 1.061 \times 10^{-4}$  lb/meg for English units.

6.6. Sulfur dioxide concentration.

$$CSO_2 = K_3 \frac{N(V_t - V_{bl}) \left( \frac{V_{soln}}{V_s} \right)}{V_m(Std)}$$

Equation 8-3

where:  
 $K_3 = 0.03333$  g/meg for metric units.  
 $= 7.061 \times 10^{-4}$  lb/meg for English units.

6.7. Isokinetic Variation.

6.7.1. Calculation from raw data.

$$I = \frac{100 T_a [K_4 V_L + (V_m/T_m) P_{bar} + \Delta H/13.6]}{60 \theta V_s P_s A_n}$$

Equation 8-4

where:  
 $K_4 = 0.003464$  mm Hg- $m^3$ /ml- $^{\circ}K$  for metric units.  
 $= 0.002876$  in. Hg- $ft^3$ /ml- $^{\circ}K$  for English units.

6.7.2. Calculation from intermediate values.

$$I = \frac{T_a V_m(Std) P_{std} 100}{T_{std} v_a \theta A_n P_s 60 (1 - B_{ws})} \\ = K_5 \frac{T_a V_m(Std)}{P_s v_a A_n \theta (1 - B_{ws})}$$

Equation 8-5

where:  
 $K_5 = 4.320$  for metric units.  
 $= 0.09450$  for English units.

6.8. Acceptable Results. If 90 percent  $\leq I \leq 110$  percent, the results are acceptable. If the results are low in comparison to the standards and  $I$  is beyond the acceptable range, the Administrator may opt to accept the results. Use Citation 4 in the Bibliography of Method 5 to make judgments. Otherwise, reject the results and repeat the test.

#### 7. Bibliography

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2. Corbett, P. E. The Determination of  $SO_2$  and  $SO_3$  in Flue Gases. Journal of the Institute of Fuel, 14:237-243, 1961.
3. Martin, Robert M. Construction Details of Isokinetic Source Sampling Equipment. Environmental Protection Agency, Research Triangle Park, N.C. Air Pollution Control Office Publication No. AP7D-4581, April, 1971.
4. Patton, W. F. and J. A. Brock, Jr. New Equipment and Techniques for Sampling Chemical Process Gases. Journal of Air Pollution Control Association, 13:162, 1963.
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7. Annual Book of ASTM Standards, Part 31; Water, Atmospheric Analysis, pp. 10-42. American Society for Testing and Materials, Philadelphia, Pa. 1974.

(Ees. 111, 114, 301a), Clean Air Act, sec. 4(a) of Pub. L. 91-604, 84 Stat. 1903; sec. 4(a) of Pub. L. 91-604, 84 Stat. 1903; sec. 2 of Pub. L. 90-148, 81 Stat. 504 [42 U.S.C. 1637c-6, 1637c-9, 1637g(a)].

[FR Doc.77-13008 Filed 8-17-77; 8:45 am]



CUSTOMER

ADDRESS

JOB NO. 800/22, CUSTOMER NO. \_\_\_\_\_, LOCATION \_\_\_\_\_RUN NO. 1007, DATE OF TEST \_\_\_\_\_

PBAR \_\_\_\_\_, VM \_\_\_\_\_, PG \_\_\_\_\_

VCB \_\_\_\_\_, VCD \_\_\_\_\_

VBF \_\_\_\_\_, VBG \_\_\_\_\_, VBH \_\_\_\_\_, VBI \_\_\_\_\_

A \_\_\_\_\_, CP \_\_\_\_\_, Y \_\_\_\_\_

WAK \_\_\_\_\_, YAJ \_\_\_\_\_, WAL \_\_\_\_\_

AN \_\_\_\_\_,  $\theta$  \_\_\_\_\_, WTT \_\_\_\_\_

UPR \_\_\_\_\_ (COMBUSTION ONLY)

Impinger Box # \_\_\_\_\_

Filter Paper # \_\_\_\_\_

Meter Box # \_\_\_\_\_

☐ Process☐ Combustion☐ Incinerator☐ English Units☐ Metric UnitsCLOCK  
TIME

POINT

GM  
READINGSTACK  
PRESS.

PITOT

STACK  
TEMP.ORIFICE  
ACT.

METER

 $T_{in}$  $T_{out}$  $\Delta P$ 

TS

 $\Delta H$ 

TAD,

TAE,

25

342.64

0.06

500

2.38

76

26

344.81

0.06

500

2.38

76

27

346.99

0.06

500

2.38

76

28

349.17

0.06

500

2.38

76

29

351.37

0.06

500

2.38

76

30

353.52

0.05

510

1.95

76

31

355.56

0.05

520

1.95

76

32

357.55

0.05

520

1.95

76

33

359.53

0.05

520

1.95

76

34

361.52

0.05

520

1.95

76

35

363.50

0.05

500

1.95

76

36

365.48

0.05

500

1.95

76

37

367.44

0.05

500

1.95

76

38

369.41

0.06

500

2.38

76

39

371.59

0.06

500

2.38

76

40

373.77

0.06

500

2.38

76

41

375.92

0.06

500

2.38

76

42

378.20

0.06

500

2.38

76

43

380.36

0.06

500

2.38

76

44

382.50

0.06

500

2.38

76

45

384.72

0.05

500

1.95

76

46

386.77

0.05

500

1.95

76

47

388.62

0.04

380

1.55

82

48

390.77

0.04

340

1.55

82

392.56

CUSTOMER Lee Black & Tite ADDRESS Summit 1110

JOB NO. 244123, CUSTOMER NO. \_\_\_\_\_, LOCATION Black Mt.

RUN NO. 1, DATE OF TEST 1/24/57

PEAR 29.86, VM 29.76, PG 0

VCB 0, VCD 10.1

VBF 1.1, VBG 0, VBH 19.3, VBI 29

A 107.28, CP 0.23, Y 1.01

WAK 201.1, YAJ -, WAL 201.1

AN 0.1275,  $\theta$  120, WTT 10.37

UPR - (COMBUSTION ONLY)

Impinger Box # 3  
Filter Paper # 12-144  
Meter Box # 1

☒ Process ☒ English Units  
☐ Combustion ☐ Metric Units  
☐ Incinerator

| CLOCK<br>TIME | POINT | GM<br>READING | STACK<br>PRESS. | PITOT      | STACK<br>TEMP. | ORIFICE<br>ACT. | METER                  |                         |
|---------------|-------|---------------|-----------------|------------|----------------|-----------------|------------------------|-------------------------|
|               |       |               |                 | $\Delta P$ | TS             | $\Delta H$      | T <sub>in</sub><br>TAD | T <sub>out</sub><br>TAE |
|               | 1     | 392.17        |                 | 0.84       | 140            | 0.84            | 78                     |                         |
|               | 2     | 398.42        |                 | 0.96       | 200            | 0.96            | 78                     |                         |
|               | 3     | 399.53        |                 | 1.10       | 230            | 1.10            | 80                     |                         |
|               | 4     | 401.62        |                 | 1.20       | 230            | 1.20            | 80                     |                         |
|               | 5     | 403.23        |                 | 1.30       | 240            | 1.30            | 80                     |                         |
|               | 6     | 404.84        |                 | 1.30       | 240            | 1.30            | 81                     |                         |
|               | 7     | 406.49        |                 | 1.40       | 240            | 1.30            | 82                     |                         |
|               | 8     | 406.19        |                 | 1.40       | 240            | 1.40            | 82                     |                         |
|               | 9     | 409.92        |                 | 1.40       | 240            | 1.40            | 82                     |                         |
|               | 10    | 411.64        |                 | 1.40       | 240            | 1.40            | 82                     |                         |
|               | 11    | 413.33        |                 | 1.40       | 240            | 1.40            | 82                     |                         |
|               | 12    | 415.04        |                 | 1.30       | 240            | 1.30            | 82                     |                         |
|               | 13    | 416.73        |                 | 1.30       | 240            | 1.30            | 82                     |                         |
|               | 14    | 418.42        |                 | 1.30       | 250            | 1.30            | 82                     |                         |
|               | 15    | 420.10        |                 | 1.30       | 250            | 1.30            | 82                     |                         |
|               | 16    | 421.79        |                 | 1.30       | 250            | 1.30            | 82                     |                         |
|               | 17    | 423.48        |                 | 1.30       | 250            | 1.30            | 82                     |                         |
|               | 18    | 425.18        |                 | 1.30       | 250            | 1.30            | 82                     |                         |
|               | 19    | 426.86        |                 | 1.30       | 250            | 1.30            | 82                     |                         |
|               | 20    | 428.55        |                 | 1.30       | 250            | 1.30            | 82                     |                         |
|               | 21    | 430.25        |                 | 1.30       | 250            | 1.30            | 82                     |                         |
|               | 22    | 431.94        |                 | 1.30       | 250            | 1.30            | 82                     |                         |
|               | 23    | 433.61        |                 | 1.20       | 250            | 1.20            | 82                     |                         |
|               | 24    | 435.30        |                 | 1.20       | 196            | 1.20            | 82                     |                         |

CUSTOMER

ADDRESS

JOB NO. \_\_\_\_\_, CUSTOMER NO. \_\_\_\_\_, LOCATION \_\_\_\_\_

RUN NO. 1007, DATE OF TEST \_\_\_\_\_

PBAR \_\_\_\_\_, VM \_\_\_\_\_, PG \_\_\_\_\_

VCB \_\_\_\_\_, VCD \_\_\_\_\_

VBF \_\_\_\_\_, VBG \_\_\_\_\_, VBH \_\_\_\_\_, VBI \_\_\_\_\_

A \_\_\_\_\_, CP \_\_\_\_\_, Y \_\_\_\_\_

WAK \_\_\_\_\_, YAJ \_\_\_\_\_, WAL \_\_\_\_\_

AN \_\_\_\_\_,  $\theta$  \_\_\_\_\_, WTT \_\_\_\_\_

UPR \_\_\_\_\_ (COMBUSTION ONLY)

|                |       |
|----------------|-------|
| Impinger Box # | _____ |
| Filter Paper # | _____ |
| Meter Box #    | _____ |

|                                      |                                        |
|--------------------------------------|----------------------------------------|
| <input type="checkbox"/> Process     | <input type="checkbox"/> English Units |
| <input type="checkbox"/> Combustion  | <input type="checkbox"/> Metric Units  |
| <input type="checkbox"/> Incinerator |                                        |

| CLOCK<br>TIME | POINT | GM<br>READING | STACK<br>PRESS. | PITOT      |     | STACK<br>TEMP. | ORIFICE<br>ACT. | METER            |                   |
|---------------|-------|---------------|-----------------|------------|-----|----------------|-----------------|------------------|-------------------|
|               |       |               |                 | $\Delta P$ | TS  |                |                 | $T_{in}$<br>TAD, | $T_{out}$<br>TAE, |
|               | 24    | 436.99        |                 | 1.20       | 220 | 1.20           |                 | 82               |                   |
|               | 26    | 438.66        |                 | 1.20       | 240 | 1.20           |                 | 82               |                   |
|               | 27    | 440.39        |                 | 1.30       | 250 | 1.30           |                 | 82               |                   |
|               | 28    | 442.12        |                 | 1.30       | 250 | 1.30           |                 | 82               |                   |
|               | 29    | 443.69        |                 | 1.30       | 250 | 1.30           |                 | 82               |                   |
|               | 30    | 445.06        |                 | 1.30       | 250 | 1.30           |                 | 82               |                   |
|               | 31    | 447.05        |                 | 1.30       | 250 | 1.30           |                 | 82               |                   |
|               | 32    | 448.72        |                 | 1.30       | 250 | 1.30           |                 | 82               |                   |
|               | 33    | 450.28        |                 | 1.30       | 250 | 1.30           |                 | 82               |                   |
|               | 34    | 452.06        |                 | 1.30       | 250 | 1.30           |                 | 82               |                   |
|               | 35    | 453.74        |                 | 1.30       | 250 | 1.30           |                 | 82               |                   |
|               | 36    | 455.41        |                 | 1.30       | 250 | 1.30           |                 | 82               |                   |
|               | 37    | 457.09        |                 | 1.30       | 250 | 1.30           |                 | 82               |                   |
|               | 38    | 458.76        |                 | 1.30       | 250 | 1.30           |                 | 82               |                   |
|               | 39    | 460.44        |                 | 1.30       | 240 | 1.30           |                 | 82               |                   |
|               | 40    | 462.12        |                 | 1.40       | 240 | 1.40           |                 | 82               |                   |
|               | 41    | 463.86        |                 | 1.40       | 240 | 1.40           |                 | 82               |                   |
|               | 42    | 465.61        |                 | 1.40       | 240 | 1.40           |                 | 82               |                   |
|               | 43    | 467.36        |                 | 1.40       | 240 | 1.40           |                 | 82               |                   |
|               | 44    | 469.09        |                 | 1.40       | 240 | 1.40           |                 | 82               |                   |
|               | 45    | 470.84        |                 | 1.20       | 240 | 1.20           |                 | 82               |                   |
|               | 46    | 472.48        |                 | 1.20       | 240 | 1.20           |                 | 82               |                   |
|               | 47    | 474.00        |                 | 1.10       | 230 | 1.10           |                 | 82               |                   |
|               | 48    | 475.57        |                 | 0.85       | 220 | 0.85           |                 | 82               |                   |

476.93

# Notch Box Calibration

1-5/75

| $\Delta H$ | $V_w$ | $V_d$ | $T_w$ | $T_d$ | $\theta$ | $\delta$ | $\Delta H_c$ |
|------------|-------|-------|-------|-------|----------|----------|--------------|
| 0.5        | 5     | 4.955 | 77    | 84    | 12:30    | 1.02     | 1.77         |
| 1.0        | 5     | 5.019 | 77    | 91    | 9:00     | 1.02     | 1.81         |
| 2.0        | 5     | 5.098 | 77    | 97    | 6:33     | 1.01     | 1.87         |
| 4.0        | 5     | 5.191 | 77    | 103   | 4:46     | 0.99     | 1.91         |

 $\bar{\delta} = 1.01$   $\Delta H_c = 1.86$ 

## 3' SS. Photo Calibration

1/20/76

| $\Delta p_{std}$ | $\Delta p_{Actual}$ | $C_p$ |
|------------------|---------------------|-------|
| 0.06             | 0.08                | 0.86  |
| 0.11             | 0.16                | 0.82  |
| 0.19             | 0.27                | 0.83  |
| 0.26             | 0.34                | 0.87  |
| 0.28             | 0.39                | 0.85  |
| 0.33             | 0.41                | 0.84  |

 $\bar{C}_p = 0.85$ 

## Nozzle Tip Calibration

| $\frac{1}{4}"$ | $\frac{3}{4}"$ | $\frac{1}{2}"$ | $\frac{1}{4}"$ |
|----------------|----------------|----------------|----------------|
| 0.251          | 0.376          | 0.502          |                |
| 0.251          | 0.374          | 0.502          |                |
| 0.247          | 0.374          | 0.501          |                |
| 0.249          | 0.377          | 0.499          |                |
| 0.250          | 0.375          | 0.499          |                |
| 0.250          | 0.375          | 0.499          |                |
| 0.251          | 0.374          | 0.499          |                |
| 0.249          | 0.376          | 0.499          |                |
| 0.249          | 0.375          | 0.499          |                |
| 0.250          | 0.375          | 0.502          |                |
| Ave 0.250      | 0.375          | 0.500          |                |

## TRAIN IN (Red)

|    | <u>Initial</u> | <u>Final</u> |
|----|----------------|--------------|
| IA | 477.1          | 444.5        |
| B  | 529.4          | 575.6        |
| C  | 424.0          | 444.4        |
| D  | 640.8          | 735.0        |

F. H. 77-143

Crain

- 52.6  
+ 46.2  
+ 20.4  
+ 44.2

+ 58.2

## TRAIN II N (Yellow)

|     |       |       |
|-----|-------|-------|
| IIA | 517.3 | 456.6 |
| B   | 534.7 | 558.0 |
| C   | 438.2 | 447.8 |
| D   | 743.0 | 788.9 |

F. H. 77-144

- 60.7  
+ 15.3  
+ 9.6  
+ 45.9

+ 10.1

*[Signature]*  
1/23/58

TITLE

800122

800123

Project No. \_\_\_\_\_

Book No. \_\_\_\_\_

From Page No. \_\_\_\_\_

Front End

Final  
Initial

1  
66.1943  
64.2547

1.9346

2  
78.7965  
78.4547

0.3418

Gain

Filter

Final  
Initial

1 (77-143)  
0.6631  
0.4188

0.2443

2 (77-141)  
0.7759  
0.4166

0.3593

Gain

Total Gain

1

2

Front  
Filter

1.9346  
0.2443

0.3418  
0.3593

Total

2.1789

0.7011

*R  
1/25/58*

To Page No

Witnessed & Understood by me

Date

Invented by

Date

Recorded by