

Note: This is a reference cited in AP 42, *Compilation of Air Pollutant Emission Factors, Volume I Stationary Point and Area Sources*. AP42 is located on the EPA web site at www.epa.gov/ttn/chief/ap42/

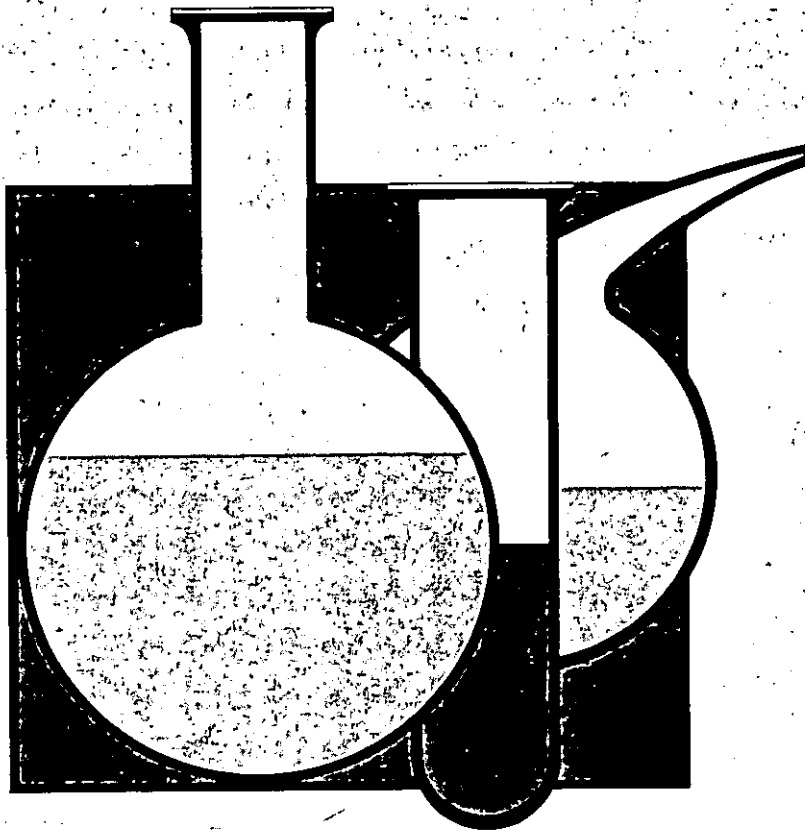
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AP42 Section:	11.3
Reference:	17
Title:	Mass Emission Tests Conducted On The #7B Tunnel Kiln In Knoxville, TN, For General Shale Products Corporation, Guardian Systems, Inc., Leeds, AL, April 22, 1986.

AP-42 Section 11.3
Reference 17

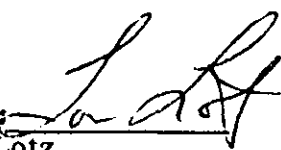
GUARDIAN SYSTEMS INC.

**P.O. Box 300
Leeds, Alabama 35094
205/699-6647**

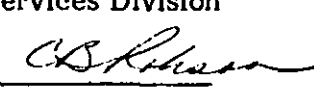


Test Report

MASS EMISSION TESTS
CONDUCTED ON THE
#7B TUNNEL KILN
IN
KNOXVILLE, TENNESSEE
FOR
GENERAL SHALE PRODUCTS CORPORATION
ON
APRIL 22, 1986

Approved by: 

Tom Lotz
Director
Field Services Division

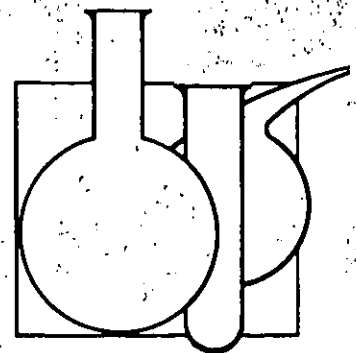
Approved by: 

C.B. Robinson, P.E.
Alabama Registration No. 9761

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Introduction



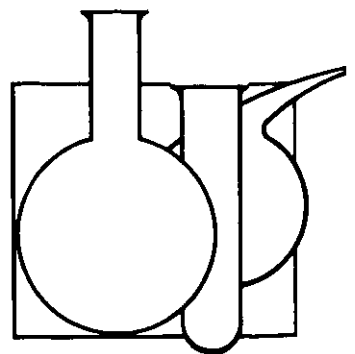
I. INTRODUCTION AND PROCESS DESCRIPTION

On April 22, 1986, Guardian Systems, Inc. performed a series of particulate emissions tests on the #7B Tunnel Kiln Stack of General Shale Products Corporation located near Knoxville, Tennessee. This unit has been modified from a dryer stack and an exhaust to only one stack. These tests were conducted in accordance to the rules and regulations expressed in the Code of Federal Regulations, Title 40, Section 60, Reference Methods 1-5 as amended.

Individual bricks are formed and stacked onto kiln cars measuring approximately 9' x 9'. Cars are inserted on a regular basis into a long, continuous-fired tunnel kiln. As one car is discharged another is inserted. This provides a constant moving mass inside the kiln. Cars are pushed through the kiln at a slow, methodical pace requiring almost three days for the complete travel (see **Plant Operational Data** for complete process information). By means of a coal firing process, heat is increased in each chamber until the total firing is complete. As the car continues through the kiln from the main firing zone the temperatures are reduced to provide necessary cooling.

Mr. Dave McNees, Corporate Representative, and Mr. Ed Bridges Plant Superintendent represented General Shale Products Corporation. Mr. T. Simon deVente, Mr. Rich Smrz, and Ms. Lynne Liddington represented the Knox County Department of Air Pollution Control. Mr. Greg Karstens and Mr. Chuck Turner, of Guardian Systems, Inc. performed these tests.

Test Results



II. SUMMARY OF TEST RESULTS

The following is a summary of the test results for Tunnel Kiln #7B conducted on April 22, 1986

Test #	1	2	3	Average
Date	4-22-86	4-22-86	4-22-86	4-22-86
Process weight, Tons/hr	See Process information			
Particulate Mass Rate, lbs/hr	12.42	14.22	13.95	13.53

*INCORRECT
SEE Pg. 9*

Source I.D. No. 0035

OBSERVER'S SUMMARY FORM

Source name General Shale Products, Corp.
City and State Knoxville, TN
Type of process Brick Tunnel Kiln 7B
Type of control equipment Innovative combustion and gases flow control
NSPS regulation and effective date N/A
Reference Method(s) and effective date(s) EPA Methods 1-5, 1 July 1985

Process Observation

Form no. N/A
Observer JS Agency Knox County Dept. of Air Pollution Control

Description of process and process operation during testing:

Process is a coal-fired brick tunnel kiln, brick laden carts are inserted at the dryer end, pass through a firing zone and exit out of a cooling zone.

The process was modified from allowing emissions to exit from two stacks to emissions exiting from a single stack.

OBSERVER'S SUMMARY FORM (continued)

Control Equipment ObservationForm no. N/AObserver DSNAgency Knox County Dept. of Air Pollution Control

Description of control equipment and control equipment operation during testing:

Emissions are reduced (particulate) by an innovative firing and exhaust control system. SO₂ is controlled by purchasing and burning low sulfur coal.

Particulate is controlled in addition by purchasing and burning a low ash coal.

Source Test ObservationForm no. N/AObserver DSNAgency Knox County Dept. of Air Pollution Control

Description of any notable occurrences:

None; process and test ran normal without any notable disruptions or shifts in processing.

Tests ran smoothly and in accordance EPA guidelines and approved by this department (KCDAPC) procedures

OBSERVER'S SUMMARY FORM (continued)

Visible Emission ObservationForm no. N/AObserver LYNNE LINDINGTON Agency Knox County Dept. of Air Pollution ControlReading ranged from 5% to 20% percent opacityMaximum average for any test 13.5% percent opacityThe source ~~was~~ was not in compliance with the opacity reading of 20% maximum at the time observations were made.Was source operating representatively during any or all violation? (If applicable) N/AOther Observations

List any items that may require attention in the future:

Process operation N/AControl equipment operation N/ATest team sampling procedures N/A

Other _____

Prepared by

A. Jindal

KCDAR

Date

22 APRIL 86

Reviewer _____

Date _____

General Shale

4-22-86

9:30am

10:00am

ADDRESS

1740 RIVERSIDE DRIVE

CITY
KNOXVILLESTATE
TNZIP
37915PHONE
522-0051

SOURCE ID NUMBER

0035

PROCESS EQUIPMENT

Kiln 7-B

OPERATING MODE

100%

CONTROL EQUIPMENT

NONE

OPERATING MODE

N/A

DESCRIBE EMISSION POINT

START Kiln stack

STOP Kiln stack

HEIGHT ABOVE GROUND LEVEL

HEIGHT RELATIVE TO OBSERVER

START 28' STOP 28'

START 24' STOP 24'

DISTANCE FROM OBSERVER

DIRECTION FROM OBSERVER

START 60' STOP 60'

START NW STOP NW

DESCRIBE EMISSIONS

START smoke

STOP smoke

EMISSION COLOR

PLUME TYPE: CONTINUOUS ☒

START offwhite STOP offwhite

FUGITIVE ☐ INTERMITTENT ☐

WATER DROPLETS PRESENT:

IF WATER DROPLET PLUME:

NO ☒YES ☐ATTACHED ☐ DETACHED ☐

POINT IN THE PLUME AT WHICH OPACITY WAS DETERMINED

START stack exit

STOP stack exit

DESCRIBE BACKGROUND

START sky

STOP sky

BACKGROUND COLOR

SKY CONDITIONS

START blue STOP blue

START STOP

WIND SPEED

WIND DIRECTION

5-7 mph

START N STOP N

AMBIENT TEMP.

WET BULB TEMP.

RH, percent

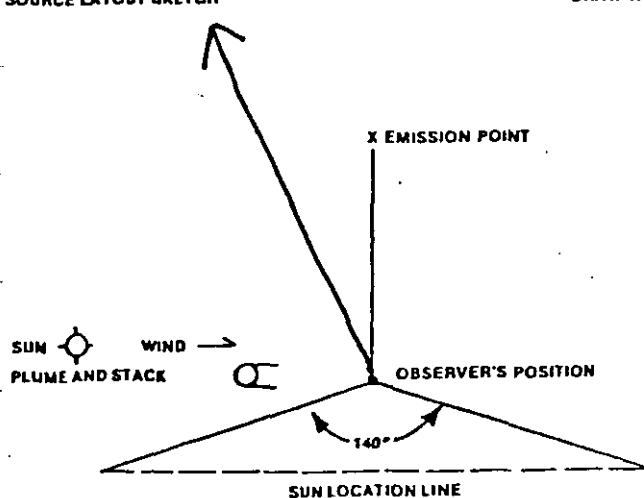
START 46°F STOP 47°F

38°F

45%

SOURCE LAYOUT SKETCH

DRAW NORTH ARROW

AVERAGE OPACITY FOR
HIGHEST PERIOD

6 minute 13.5%

NUMBER OF READINGS ABOVE

20 % WERE 0

RANGE OF OPACITY READINGS

MINIMUM 5

MAXIMUM 15

OBSERVER'S NAME (PRINT)

LYNDE LIDDINGTON

OBSERVER'S SIGNATURE

DATE

4-22-86

ORGANIZATION

KCHPC

CERTIFIED BY

Carl Koontz

DATE

4-15-86

VERIFIED BY

DATE

SOURCE NAME

General Shale

ADDRESS

1740 RIVERSIDE DRIVE

CITY

Knoxville

STATE

TN

ZIP

37915

PHONE

522-0051

SOURCE ID NUMBER

0035

PROCESS EQUIPMENT

Kiln 7-B

OPERATING MODE

100%

CONTROL EQUIPMENT

none

OPERATING MODE

N/A

DESCRIBE EMISSION POINT

START Kilnstack

STOP Kilnstack

HEIGHT ABOVE GROUND LEVEL

HEIGHT RELATIVE TO OBSERVER

START 28' STOP 28'

START 24' STOP 24'

DISTANCE FROM OBSERVER

DIRECTION FROM OBSERVER

START 60' STOP 60'

START NW STOP NW

DESCRIBE EMISSIONS

START smoke

STOP smoke

EMISSION COLOR

PLUME TYPE: CONTINUOUS ☒

START offwhite STOP offwhite

FUGITIVE ☐ INTERMITTENT ☐

WATER DROPLETS PRESENT:

IF WATER DROPLET PLUME:

NO ☒YES ☐ATTACHED ☐ DETACHED ☐

POINT IN THE PLUME AT WHICH OPACITY WAS DETERMINED

START stack exit

STOP stack exit

DESCRIBE BACKGROUND

START sky

STOP sky

BACKGROUND COLOR

SKY CONDITIONS

START blue STOP blue

START scattered clouds STOP scattered clouds

WIND SPEED

WIND DIRECTION

START 5-7mph STOP 5-7mph

START NE STOP NE

AMBIENT TEMP.

WET BULB TEMP.

RH, percent

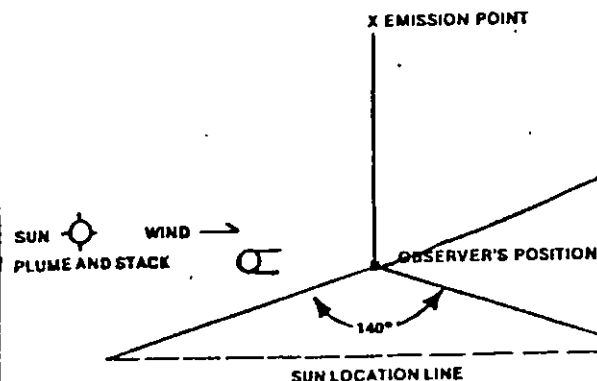
START 53°F STOP 54°F

44°F

46%

SOURCE LAYOUT SKETCH

DRAW NORTH ARROW



COMMENTS

STACK TEST

Run #3

* Door opened

4-22-86

1:26pm

1:56

SEC	0	15	30	45	SEC	0	15	30	45
MIN					MIN				
1	10	10	5	10	31				
2	10	10	5	10	32				
3	10	10	10	10	33				
4	10	10	10	10	34				
5	10	10	10	5	35				
6	5	5	10	10	36				
7	10	10	*10	10	37				
8	10	10	15	15	38				
9	15	20	20	20	39				
10	15	10	10	10	40				
11	5	5	5	5	41				
12	5	5	5	5	42				
13	5	5	10	10	43				
14	5	5	10	10	44				
15	10	10	15	15	45				
16	10	5	5	10	46				
17	5	5	5	5	47				
18	5	10	10	10	48				
19	10	10	5	10	49				
20	10	10	10	15	50				
21	10	15	10	10	51				
22	15	10	10	15	52				
23	10	10	10	10	53				
24	10	10	15	15	54				
25	15	15	10	10	55				
26	15	10	15	10	56				
27	10	10	10	10	57				
28	10	10	5	5	58				
29	5	5	5	15	59				
30	15	15	15	15	60				

1st 6 minute

Average opacity
= 8.9%

2nd 6 minute

Average opacity
= 10.4%

3rd 6 minute

Average opacity
= 8.1%

4th 6 minute

Average opacity
= 11%

5th 6 minute

Average opacity
= 10.8%AVERAGE OPACITY FOR
HIGHEST PERIOD
6 minutes

11%

NUMBER OF READINGS ABOVE

20 % WERE 0

RANGE OF OPACITY READINGS

MINIMUM

MAXIMUM 20

OBSERVER'S NAME (PRINT)

LYNNE LIDDINGTON

OBSERVER'S SIGNATURE

Lynne Liddington

DATE

4-22-86

ORGANIZATION

KCAPC

CERTIFIED BY

Carl Koontz

DATE

4-15-86

VERIFIED BY

DATE

GUARDIAN * SYSTEMS * INCORPORATED

P.O. BOX 300
LEEDS, AL 35094
205-699-6647

Summarized Air Test Results for General Shale Products

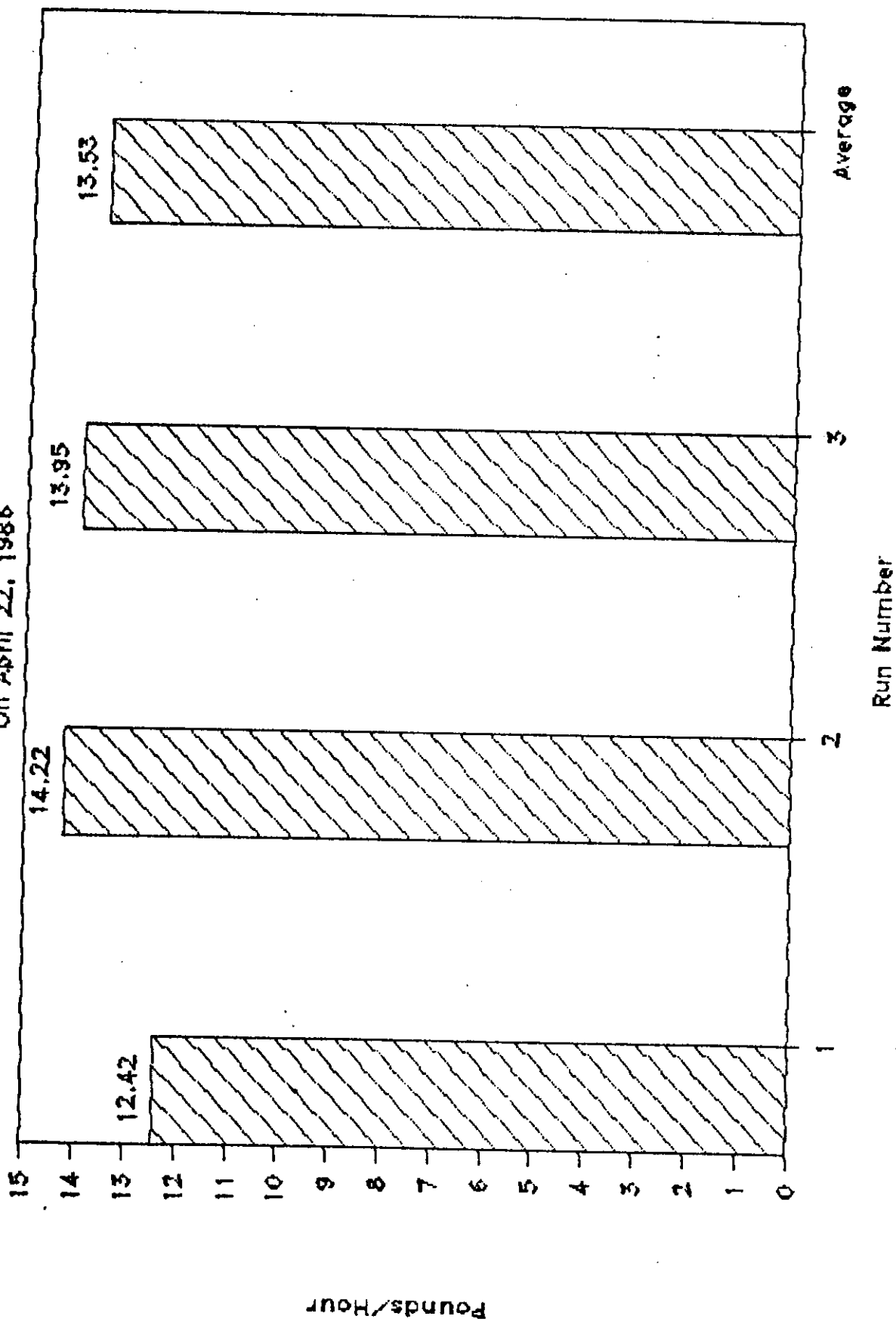
Run Number	1	2	3	Average
Date	4-22-86	4-22-86	4-22-86	4-22-86
Location	Stack	Stack	Stack	Stack
Time	0929-1035	1123-1230	1328-1435	0929-1435
Stack Gas Temperature, F	174	175	164	171
Moisture Content, % v/v	5.29	6.30	6.97	6.20
Oxygen Content, % v/v	18.00	18.00	18.00	18.00
Carbon Dioxide Content, % v/v	2.00	2.00	2.00	2.00
Carbon Monoxide Content, % v/v	0.00	0.00	0.00	0.00
Excess Air, %	576.92	576.92	576.92	576.92
Stack Gas Velocity Feet per Second	66.78	66.97	67.69	67.15
Volumetric Flow Actual Cubic Feet per Minute	28,329	28,407	28,715	28,485
Volumetric Flow Dry Std Cubic Feet per Minute	22,372	22,159	22,629	22,384
Concentration Grains per Actual Cubic Foot	0.065	0.075	0.072	0.071
Concentration Grains per Dry Std Cubic Ft	0.051	0.058	0.057	0.055
Particulate Mass Rate, #/hr	12.42	14.22	13.95	13.53
% Isokinetic	101.54	103.46	103.64	102.90

Gr / ACF * DSCFM

INCORRECT

GENERAL SHALE PRODUCTS MASS EMISSIONS

On April 22, 1986



GUARDIAN * SYSTEMS * INCORPORATED
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205-699-6647

Computer Input Parameters for General Shale Products

Run Number	1	2	3	Average
Date	4-22-86	4-22-86	4-22-86	4-22-86
Location	Stack	Stack	Stack	Stack
Time	0929-1035	1123-1230	1328-1435	0929-1435
Barometric Pressure, in Hg	29.96	29.96	29.96	29.96
Static Pressure, in H2O	-0.070	-0.070	-0.070	-0.070
Run Time, minutes	60.00	60.00	60.00	180.00
Meter Volume, CF	33.220	33.851	34.756	
Meter Correction factor, MCF	0.9948	0.9948	0.9948	
Meter Volume (Corrected)	33.047	33.675	34.575	101.297
Stack Temperature, F	174	175	164	171
Meter Temperature, F	54	59	61	58
Meter Pressure, in H2O	0.9	0.9	0.96	0.92
Sqr Velocity Pressure	1.090	1.090	1.110	1.097
Mass of Particulate, mg	143.3	167.1	164.2	474.6
Ml of Water Collected	40.4	49.1	56.0	145.5
% Oxygen	18.00	18.00	18.00	18.00
% Carbon Dioxide	2.00	2.00	2.00	2.00
% Carbon Monoxide	0.00	0.00	0.00	0.00
Stack Area, Sq ft	7.070	7.070	7.070	7.070
Pitot Correction Factor	0.831	0.831	0.831	0.831
Nozzle Diameter, in	0.180	0.180	0.180	0.180

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205-699-6647

Computed Air Test Results for General Shale Products

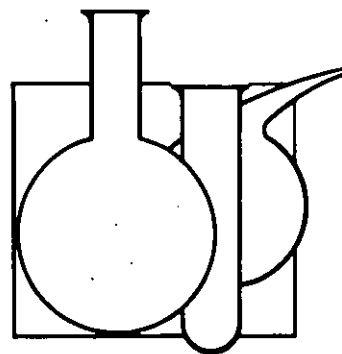
Run Number	1	2	3	Average
Date	4-22-86	4-22-86	4-22-86	4-22-86
Location	Stack	Stack	Stack	Stack
Time	0929-1035	1123-1230	1328-1435	0929-1435
1. Stack Pressure				
Inches Hg	29.95	29.95	29.95	29.95
Millimeters Hg	760.85	760.85	760.85	760.85
2. Meter Pressure				
Inches Hg	30.03	30.03	30.03	30.03
Millimeters Hg	762.66	762.66	762.78	762.70
3. Meter Volume				
Dry Std Cubic Feet	34.068	34.381	35.169	103.625
Dry Std Cubic Meters	0.965	0.974	0.996	2.935
4. Water Volume				
Std Cubic Feet	1.902	2.311	2.636	6.849
Std Cubic Meters	0.054	0.065	0.075	0.194
5. Moisture Content, %	5.29	6.30	6.97	6.20
6. Molecular Weight Dry	29.04	29.04	29.04	29.04
7. Molecular Weight Weight	28.46	28.34	28.27	28.36
8. Stack Velocity				
Feet per Second	66.78	66.97	67.69	67.15
Meters per Second	20.36	20.41	20.63	20.47
9. Volumetric Flow				
Actual Cubic Ft per minute	28,329	28,407	28,715	28,485
Actual Cubic M per second	13.37	13.41	13.55	13.45
10. Volumetric Flow				
Dry Std Cubic Ft per minute	22,372	22,159	22,629	22,384
Dry Std Cubic M per minute	10.56	10.46	10.68	10.57
11. Concentration				
Grains per Dry Std Cubic Ft	0.0648	0.0748	0.0719	0.0705
Grams per Dry Std Cubic M	0.1482	0.1713	0.1645	0.1614
12. Excess Air, %	576.92	576.92	576.92	576.92

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Computed Air Test Results for General Shale Products

Run Number	1	2	3	Average
Date	4-22-86	4-22-86	4-22-86	4-22-86
Location	Stack	Stack	Stack	Stack
Time	0929-1035	1123-1230	1328-1435	0929-1435
15. Particulate Mass Rate Pounds per Hour, #/hr	12.42	14.22	13.95	13.53
16. Volume at Nozzle Actual Cubic Feet	43.142	44.078	44.629	131.875
Actual Cubic Meters	1.222	1.248	1.264	3.735
17. Concentration Grains per Actual Cubic Ft	0.0512	0.0584	0.0567	0.0554
Grams per Actual Cubic M	0.1171	0.1336	0.1297	0.1268
18. Isokinetic, %	101.54	103.46	103.64	102.90

Sampling & Analytical Procedures



III. SAMPLING AND ANALYTICAL PROCEDURES

General

All sampling and analytical procedures for determination of the particulate emissions from this source were conducted in strict adherence with the Code of Federal Regulations, Title 40, Part 60, Appendix A, Methods 1-5 as amended. The equipment used in this test was manufactured by Research Appliance Corporation and was properly calibrated before these tests (See **Calibrations**). The particulate mass was determined gravimetrically after removal of uncombined water.

METHOD 1

This method was used to determine the number of sampling points and the required matrix. The dimensions of the stack (see **Figure 1**) indicated that 20 points would be required to sample this source. We sampled 20 points (10 per diameter). Verification of absence of cyclonic flow was determined as requested by Knox County and the results indicated that cyclonic flow did not seem to exist from the stack exhaust.

METHOD 2

Velocity measurements were taken using a properly calibrated S type pitot tube and a 0-10 inch inclined manometer.

METHOD 3

Gas analysis for CO_2 , O_2 , and N_2 by difference was performed by using the grab sample technique twice during each test and analyzed with a Fyrite Gas Analyzer (0-20% scale with 0.5% divisions).

METHOD 4

Moisture content of the stack gases was determined in conjunction with Method 5 for each test by weighing the amount of water collected in the impingers and the increase in weight of the silica gel. These weights were combined to give the total amount of water collected.

METHOD 5

Sampling Techniques

An initial velocity traverse was performed to determine stack temperature, pressure, range of velocity heads, moisture content and stack gas dry molecular weight prior to sampling. A Monroe 1830 programable calculator or a Radio Shack PC-4 computer and a TI55 was used to calculate the sampling rate for isokinetic sampling. The particulate determinations were made by utilizing the sample train in **Figure 2**. The meter box was leak checked from the pump to the orifice and initial and final leak checks of the sampling system and pitot lines were performed as outlined in Method 5 and were recorded on the data sheets (**See Field Data**). The nozzle (stainless steel 316 with an angle of taper of 30° and of button hook design) was calibrated before and after each test using a micrometer and was also recorded on the data sheets.

The sampling probe was placed at each sampling point for three minutes to provide a total sampling time of 60 minutes for each of the three tests. The gases were drawn through a stainless steel nozzle attached to a heated glass lined probe. The probe was maintained at the proper setting to obtain an exit temperature of 248 ± 25 °F (**See Calibrations**). The gases then pass through a glass fiber filter (Gelman, Class A) of 0.3 micron retention to remove particulate matter. The filter was maintained at a temperature of 248 ± 25 °F. These temperatures were recorded at each point on the data sheets.

The gases were then pass through a condenser placed in an ice bath to maintain a maximum exit temperature of 68° F. This temperature was also recorded on the data sheets. The clean and cool gases then entered the meter box where the gas flow and temperature were measured and recorded. (**See Field Data**)

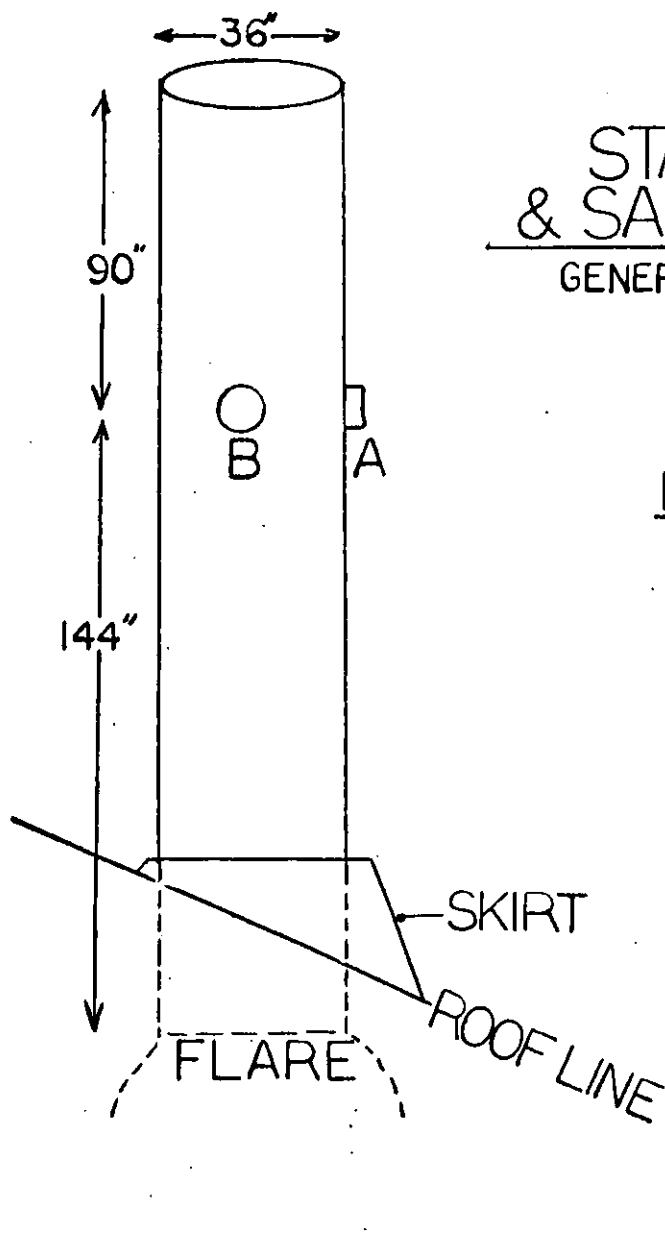
Upon completion of the sampling the sampling probe was removed from the stack and the post-test meter and pitot leakage rates were determined and recorded on the Data Sheets. The complete sampling train was transfered to the cleanup area making sure no sample was lost. The cleanup data was recorded on **Particulate Sample Recovery and Intergrity Sheet** located in the Field Data Section.

Particulate catches were placed in sealed petri dishes. Each acetone rinse from the nozzle, probe, and filter holder was combined and placed in a sealed container. For the group of tests an acetone blank of approximately 200 milliliters was placed in a sealed container. These containers were clearly marked and transported to our laboratory for analysis.

Analysis

The Filter (Gelman, Class A, without organic binder, minimum 99.9% retention for particules of 0.3 microns as determined by DOP tests) were prepared for the field test by first heating for 2 hours 220°F then desiccating at $68 \pm 10^{\circ}\text{F}$ at ambient pressure for 24 hours and weighing at intervals of at least six (6) hours to a constant weight to the nearest 0.1 milligrams (less than 0.5 milligrams change from previous reading). Upon return to the laboratory, the filters were subjected to the same procedures as outlined above. The weights were recorded in a bound laboratory book and transferred to the sheets in this report (**Method 5 Train Analytical Particulate Data**). During each weighing the filter was not exposed to laboratory atmosphere for more than two (2) minutes and a relative humidity of less than fifty percent (50%).

The acetone (reagent grade, 0.001 % residue, in glass bottles) blank (**Blank Analytical Data**) for the group of tests and the acetone rinses for each test were evaporated to dryness in tared glass beakers. They were then desiccated for twenty-four (24) hour and weighed to a constant weight as describe above.

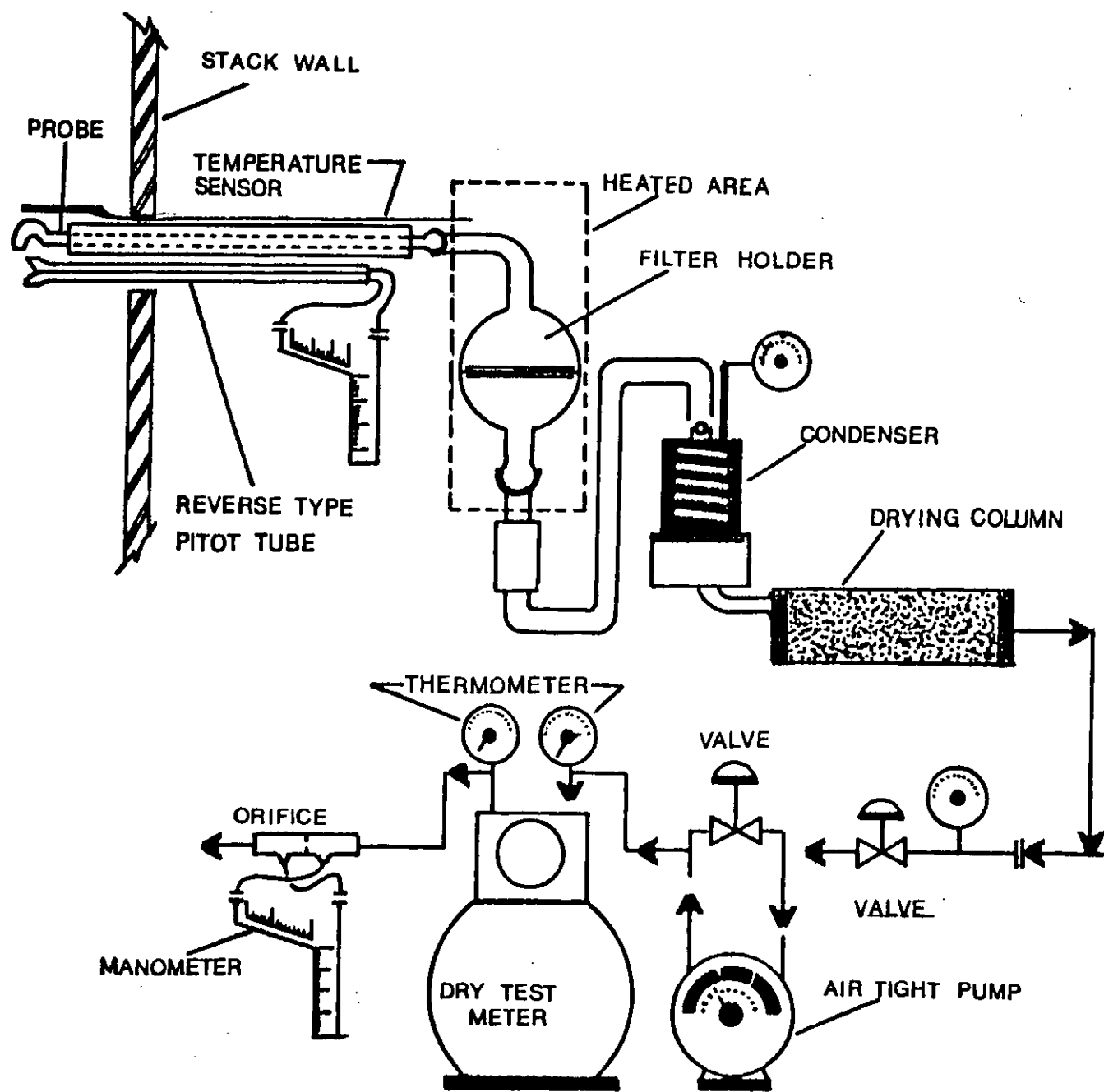


STACK BREECHING & SAMPLING LOCATIONS

GENERAL SHALE : KNOXVILLE, TN.

<u>POINT</u>	<u>INCHES TO WALL</u>
1	6
2	7.9
3	10.3
4	13.1
5	17.3
6	28.7
7	32.9
8	35.7
9	38.1
10	40

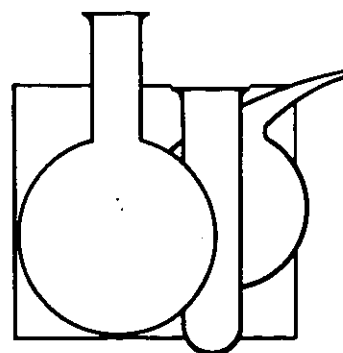
Figure 1



PARTICULATE SAMPLING TRAIN.. METHOD 5

FIGURE 2

Field Data



NOMENCLATURE

ACF - Actual Cubic Feet

ACFM - Actual Cubic Feet per minute

ACM - Actual Cubic Meters

ACMS - Actual Cubic Meters per second

An - Cross sectional area of nozzle, (ft²)

As - Area of Stack, (ft²)

Bws - Water vapor in the gas stream, proportion by volume
(dimensionless)

Ca - Acetone blank residue concentration, mg/g

c_a - Particulate Concentration, ACF

CFM - Cubic feet per minute

Cp - Pitot tube coefficient, (dimensionless)

c_s - Particulate Concentration, grains/DSCF

Cso₂ - Concentration of sulfur dioxide (dry basis) corrected
to standard conditions, lb/DSCF

C₁₂ - Particulate concentration (c_s adjusted to 12% excess air),
grains/DSCF

C₅₀ - Particulate concentration (c_s adjusted to 50% excess air),
grains/DSCF

DSCF - Dry Standard Cubic Feet

DSCFM - Dry Standard Cubic Feet per minute

DSCM - Dry Standard Cubic Meters

DSCMS - Dry Standard Cubic Meters per second

EA - Excess Air, %

I - Isokinetic Sampling, %

Km - Orifice Correction Factor, (dimensionless)

Kp - Pitot tube constant, 85.49 $\left[\frac{(\text{lb/lb-mole})(\text{in. Hg})}{(^{\circ}\text{R})(\text{in. H}_2\text{O})} \right]^{1/2}$

NOMENCLATURE - continued

- La - Maximum acceptable leakage rate for either a pretest leak check or for a leak check following a component change; equal to 0.02 CFM or 4 percent of the average sampling rate, whichever is less.
- Li - Individual leakage rate observed during the leak check conducted prior to the "ith" component change ($i = 1, 2, 3, \dots, n$), CFM.
- Lp - Leakage rate observed during the post test leak check, $\text{ft}^3/\text{min. (cfm)}$.
- Ma - Mass of residue of acetone after evaporation, mg.
- Md - Molecular weight of stack gas; dry basis, lb/lb-mole.
- Mn - Total amount of particulate matter collected, mg.
- Ms - Molecular weight of stack gas; wet basis, lb/lb-mole.
- Mw - Molecular weight of water, 18.0 g/g-mole (18.01 lb/lb-mole)
- ΔP - Velocity head of stack gas, in. H_2O
- Pa - Density of acetone, mg/ml
- Pbar - Barometric pressure at the sampling site, in. Hg
- Pg - Stack static pressure, in. H_2O
- Pm - Meter pressure, in. Hg
- PMR - Particulate Mass Rate, lbs per hour
- Ps - Absolute stack pressure, in. Hg
- Pstd - Standard absolute pressure, 29.92 in. Hg
- Pw - Density of water, 0.9982 g/ml (0.002201 lb/ml)
- Qa - Volumetric flow rate, ACFM
- Qs - Volumetric flow rate, DSCFM
- R - Ideal gas constant, 0.06236 mm Hg - $\text{m}^3/\text{°K-g-mole}$
(21.85 in. Hg- $\text{ft}^3/\text{°R-lb-mole}$)
- SCF - Standard Cubic Foot
- ta - Ambient Temperature, $^{\circ}\text{F}$
- tm - Average Temperature of meter, $^{\circ}\text{F}$
- ts - Average Temperature of stack, $^{\circ}\text{F}$

NOMENCLATURE - continued

tstd - Standard Temperature, 68°F

NOTE: Capital "T" denotes degrees Rankin

Va - Volume of acetone blank, ml

Vaw - Volume of acetone used in wash, ml

Vlc - Total volume of liquid collected in condenser and silica gel, ml

Vm - Volume of gas sample, as measured by the dry gas meter, ACF

Vmc - Volume of gas sample, corrected for leak, ACF

Vm(std) - Volume of gas sample measured by the dry gas meter, corrected to standard conditions, DSCF

Vn - Volume collected at stack conditions through nozzle, ACF

Vs - Average stack gas velocity, ft/sec.

Vw(std) - Volume of water in the gas sample, corrected to standard conditions, SCF

Wa - Weight of residue in acetone wash, mg

Y - Dry gas meter calibration factor, (dimensionless)

ΔH - Average pressure differential across the calibrated orifice, in. H₂O

ΔH_a - Value of ΔH measured for a specific orifice when operated under the following conditions: 0.75 cfm of dry air (M.W. = 29) at 68°F, 29.92 in. Hg.

$\sqrt{\Delta P}$ - Average of the square roots of the velocity pressure, in. H₂O

θ - Total sampling time, min.

θ_1 - Sampling time interval from the beginning of a run until the first component change, min.

θ_i - Sampling time interval between two successive component changes, beginning with the interval between the first and second changes, min.

θ_p - Sampling time interval from the final (n^{th}) component change until the end of the sampling run, min.

%CO₂, %O₂, %N₂, %CO - Number percent (%) by volume (dry basis) of each compound in the stack gas.

EQUATIONS

$$1. \quad P_s = P_{\text{bar}} + \frac{P_g}{13.6}$$

$$2. \quad P_m = P_{\text{bar}} + \frac{\Delta H}{13.6}$$

$$3. \quad V_{m(\text{std})} = V_m Y \left(\frac{T_{\text{std}}}{T_m} \right)$$

$$\left[\frac{P_{\text{bar}} + \frac{\Delta H}{13.6}}{P_{\text{std}}} \right]$$

$$4. \quad V_w(\text{std}) = 0.04707 V_{1c}$$

$$5. \quad B_{ws} = \frac{V_w(\text{std})}{V_{m(\text{std})} + V_w(\text{std})}$$

$$6. \quad M_d = 0.44 (\%CO_2) + 0.32 (\%O_2) + 0.28 (\%N_2 + \%CO)$$

$$7. \quad M_s = M_d (1 - B_{ws}) + 18(B_{ws})$$

$$8. \quad v_s = K_p C_p (\sqrt{\Delta p}) \text{ avg.}$$

$$\sqrt{\frac{T_s}{M_s P_s}}$$

$$9. \quad Q_a = (v_s) (A_s) (60)$$

$$10. \quad Q_s = Q_a (1 - B_{ws}) \left(\frac{528}{T_s} \right) \left(\frac{P_s}{29.92} \right)$$

$$11. \quad c_s = [0.0154 (Mn/V_{m\text{std}})]$$

$$12. \quad EA = \left[\frac{\%O_2 - 0.5 \%CO}{0.264 \%N_2 (\%O_2 - 0.5 \%CO)} \right] 100$$

$$13. \quad c_{50} = \frac{c_s}{1 - \left[\frac{(1.5)(\%O_2) - 0.133(\%N_2) - 0.75 (\%CO)}{21} \right]}$$

$$14.. \quad c_{12} = c_s \frac{12}{\%CO_2}$$

EQUATIONS - continued

$$15. \quad \text{PMR} = (c_s)(Q_s) \left(\frac{60}{7000} \right)$$

$$16. \quad V_n = \frac{T_s}{P_s} \left[(0.002669)(V_{1c}) + \frac{V_m}{T_m} \left(P_{\text{bar}} + \frac{\overline{\Delta H}}{13.6} \right) \right]$$

$$17. \quad C_a = (0.0154)(M_n) / V_n$$

$$18. \quad I = \frac{100 V_n}{60 \theta v_s A_n}$$

$$19. \quad V_{mc} = V_m - (L_p - L_a) \theta$$

$$20. \quad W_a = C_a V_{aw} p_a$$

METHOD 2 GAS VELOCITY AND VOLUME DATA

PLANT AND CITY		RUN DATE		
1.	General Shale / Knoxville	04	22	86

SAMPLING LOCATION	CLOCK TIME 0830

RUN NUMBER	OPERATOR	AMB. TEMP. (°F)	BAR. PRESS (in. Hg)	STATIC PRESS (in. H ₂ O)
1	Turner/Karstens	49°	29.96	-.07

MOLECULAR WT.	STACK INSIDE DIMENSION (in.)		PITOT TUBE Cp
	DIAM OR SIDE 1	SIDE 2	
	3.6" ID	3.6" ID	8.4

FIELD DATA

TRAVERSE POINT NUMBER	POSITION (in.)	VELOCITY HEAD (Δp_s), in. H_2O	STACK TEMP., °F	CYCLONIC FLOW DETERMINATION	
				Δp_s at 0° REFERENCE	ANGLE (α) WHICH YIELDS A NULL Δp
A 1	5.9	0	172	0	1°
2	7.4	0	172	0	1°
3	10.3	0	173	0	0°
4	13.1	0	173	0	2°
5	17.1	0	175	0	3°
6	22.7	0	176	0	8°
7	32.9	0	177	0	9°
8	35.7	0	177	0	6°
9	36.1	0	176	0	3°
10	40.1	0	176	0	1°
B 1	5.9	0	172	0	1°
2	7.4	0	171	0	3°
3	10.3	0	171	0	2°
4	13.1	0	171	0	2°
5	17.3	0	171	0	3°
6	22.7	0	172	0	3°
7	32.7	0	172	0	0°
8	35.7	0	172	0	0°
9	38.1	0	171	0	0°
10	40.1	0	172	0	1°
AVERAGE ANGLE (α)					2.4°

Average of (α) must be less than 10 degrees to be acceptable:

FIELD DATA SHEET

GUARDIAN SYSTEMS INC.

PLANT

GEN SHALE

RUN #

#1

LOCATION

KNOXVILLE

DATE

4-22-86

BOX 300

LEEDS, ALABAMA 35094

BARO. PRES.

29.96

TIME

0929-1035

	TIME		METER VOL FT 3	STACK TEMP OF	METER TEMP. OF			IMP TEMP OF	BOX TEMP OF	METER PRESSURE "H2O	VELOCITY PRESSURE "H2O	VACUUM PRESSURE "Hg	STATIC PRESSURE "H2O	
	MIN	OUR			IN	OUT	AVG						- .07	
			2475.478										PROBE TIP SIZE	
													BEFORE	AFTER
A													.180	.180
1	3	3	477.3	162	50	50	50	37	235	.93	1.22	2.1	.180	.180
2		6	478.9	170	54	50	52	38	236	.90	1.20	2.0	.180	.180
3		9	480.4	173	56	51	53	37	238	.81	1.08	1.8		
4		12	482.2	175	56	51	53	38	241	.78	1.05	6.5	#7	
5		15	483.6	177	57	52	54	38	239	.81	1.08	1.9	ml.	35
6		18	485.4	178	56	50	53	39	238	.92	1.24	5.4	gram	75.4
7		21	487.0	178	57	51	53	39	241	.88	1.18	3.4	Total	40.4
8		24	488.7	177	57	51	53	38	239	.82	1.10	2.4	OPERATOR	
9		27	490.3	177	57	52	54	38	238	.90	1.20	2.6	KARSTENS-	
10		30	491.8	173	57	52	54	38	236	.62	.82	2.5	TURNER	
B													Sample Box No.	7002
1	3	33	493.4	173	55	51	53	37	231	.86	1.15	2.4	Meter Box No.	700
2		36	494.9	170	56	51	53	38	231	.97	1.29	2.7	Meter ΔH@	1.66
3		39	496.6	166	56	51	53	38	230	.99	1.30	2.6	Pitot, CP	.84
4		42	498.5	171	57	52	54	38	230	.96	1.28	2.7	Temp. Device	STILL
5		45	500.5	172	58	52	55	38	230	1.00	1.33	2.8	Probe No.	S-N
6		48	501.8	176	59	53	56	38	229	.94	1.25	2.4	Probe Liner	GLASS
7		51	504.2	175	60	53	56	38	228	.92	1.23	2.6	Probe Htr. Set	507.0
8		54	505.5	176	60	53	56	38	230	.98	1.30	3.1	Ambient Temp.	48°
9		57	506.8	177	61	53	57	38	230	.95	1.26	3.1	% O ₂	18 18
10		60	508.698	177	61	53	57	38	230	.98	1.31	3.4	% CO ₂	2 2
20		60	33.220	174			54			.896	1.09		NOTES	
													Orifice	✓ at 18" H ₂
													Pitot	✓
													Meter	✓ at 18" H ₂
													S 5.2 for 15 sec	
													R 6.8 " " "	
													FINAL	
													S 5.6 for 15 sec	
													R 5.7 " "	
													508.744 Final low	
													508.744 0.4	

FIELD DATA SHEET

GUARDIAN SYSTEMS INC.

BOX 300
LEEDS, ALABAMA 35094

AC

PLANT

GEN SHALE

RUN # 2

LOCATION

KNOXVILLE

DATE

4-22-86

BARO. PRES.

29.96

TIME

1123-1230

	TIME		METER VOL FT 3	STACK TEMP OF	METER TEMP. OF			IMP TEMP OF	BOX TEMP OF	METER PRESSURE H ₂ O	VELOCITY PRESSURE H ₂ O	VACUUM PRESSURE H _g	STATIC PRESSURE "H ₂ O"	
	MIN	DUR			IN	OUT	AVG						BEFORE	AFTER
			508.825											
B				(1)	(2)	(3)		(4)	(5)					
1	3	3	510.5	167	51	51	51	36	242	.94	1.25	1.0	.180	.180
2		6	512.2	171	52	52	52	40	269	.92	1.23	1.1	.180	.180
3		9	514.0	172	55	53	54	40	265	.98	1.30	1.1	.180	.180
4		12	516.1	173	57	53	55	39	248	.98	1.30	1.2		
5		15	517.6	175	58	53	56	40	258	.99	1.32	1.4		
6		18	519.2	177	60	54	57	41	231	.92	1.22	1.4		
7		21	520.9	178	61	54	57	40	242	.90	1.20	1.5		
8		24	522.6	179	61	54	57	41	244	.88	1.18	1.5		
9		27	524.2	175	63	55	59	42	248	.92	1.21	1.8		
10		30	525.9	175	65	56	60	40	226	.81	1.07	1.4		
A														
1	3	33	527.7	165	63	57	60	35	229	.99	1.28	1.9		
2		36	529.5	180	65	57	61	41	238	.92	1.21	1.9		
3		39	531.1	177	66	59	62	43	246	.89	1.18	2.0		
4		42	532.7	179	66	59	62	43	254	.85	1.12	1.8		
5		45	534.4	178	65	60	62	44	263	.87	1.15	2.0		
6		48	536.3	177	66	61	63	44	257	.97	1.28	2.1		
7		51	538.1	177	67	60	63	41	238	.95	1.25	2.1		
8		54	539.8	176	65	59	62	40	234	.91	1.20	2.0		
9		57	541.2	174	66	60	63	42	237	.74	.97	1.7		
10		60	542.676	172	66	60	63	42	241	.64	.84	1.5		
20		60	33.851	175			59			.90	1.09			

PROBE TIP SIZE

BEFORE AFTER

.180 .180
 .180 .180
 .180 .180

#3 WATER

ml. 43

gram 6.1

Total 49.1

OPERATOR

KARSTENS

TURNER

Sample Box No. 2

Meter Box No. 700

Meter ΔH@ 1.66

Pitot, CP .81

Temp. Device 244

Probe No. S-N

Probe Liner 644

Probe Htr. Set 50.2

Ambient Temp. 51°

% O₂ 18 18% CO₂ 2 2

NOTES

Orifice

Pitot

Meter

3.8 St

5.1 Ram

Leak ✓ at .005

S 3.8

R 4.4 at 3.44

542.685 SMR

542.689 FMM

.004

FIELD DATA SHEET

PLANT General ShaleRUN # 3

GUARDIAN SYSTEMS INC.

LOCATION KnoxvilleDATE 4/22/86BOX 300
LEEDS, ALABAMA 35094BARO. PRES. 29.96TIME 1328-1425

	TIME		METER VOL FT 3	STACK TEMP OF	METER TEMP. OF			IMP TEMP OF	BOX TEMP OF	METER PRESSURE "H ₂ O	VELOCITY PRESSURE "H ₂ O	VACUUM PRESSURE "Hg	STATIC PRESSURE "H ₂ O	
	MIN	DUR			IN	OUT	AVG						BEFORE	AFTER
					(1)	(2)	(3)		(4)	(5)				
A	3	8	542.748											
1	3	3	544.5	170	55	55	55	36	230	.97	1.28	2.2	.180	.180
2	6	6	546.2	176	56	56	56	37	240	.91	1.21	2.3	.180	.180
3	9	9	548.0	150	58	56	57	38	248	1.02	1.30	2.3	.180	.180
4	12	12	549.6	164	60	56	58	39	252	.88	1.13	2.2		
5	15	15	551.3	160	60	58	59	39	257	.94	1.21	2.1		
6	18	18	553.2	163	61	57	59	39	256	1.03	1.34	2.1		
7	21	21	554.9	165	63	57	60	40	265	1.07	1.35	3.0		
8	24	24	556.6	167	64	58	61	40	266	1.00	1.30	2.9		
9	27	27	558.4	169	64	58	61	40	267	.95	1.24	3.1		
10	30	30	559.7	166	65	58	61	40	268	.77	1.0	2.9		
11	33	33	561.7	165	64	59	61	38	271	1.01	1.31	2.8		
12	36	36	563.5	173	65	59	62	40	263	.99	1.30	2.9		
13	39	39	565.3	174	66	60	63	38	262	.98	1.28	2.9		
14	42	42	566.9	176	66	60	63	39	268	.98	1.29	2.9		
15	45	45	569.0	178	67	61	64	40	252	1.16	1.45	3.6		
16	48	48	570.9	157	68	62	64	41	248	1.02	1.29	3.5		
17	51	51	572.6	161	67	62	65	42	241	.96	1.23	3.5		
18	54	54	574.4	164	67	62	65	40	264	.94	1.21	3.5		
19	57	57	575.9	164	67	63	65	39	271	.76	.98	3.1		
20	60	60	577.504	158	66	62	64	40	263	.83	1.05	3.5		
21	60	60	34.756	164			61			.957	1.11			

WATER
#2
ml. 50
gram 6
Total 56

OPERATOR
Turner / Karstens

Sample Box No. 2
Meter Box No. 700
Meter ΔH@ 1.66
Pitot, CP .84
Temp. Device RTD
Probe No. 5N
Probe Liner glass
Probe Htr. Set 60%
Ambient Temp. 60°
% O₂ 18 / 18
% CO₂ 2 / 2

NOTES
Orifice ☒
Pitot ☒
Meter ☒
S-4.5 for 15 sec
R-5.1 " " "
Leak ☒ .004
at 15" Hg

S 3.8
R 4.8 AT 4" Hg
577.5205 mm
577.524
.008

BLANK ANALYTICAL DATA

Plant GENERAL SHALE
 Sample location KNOXVILLE
 Relative humidity 20%
 Type of blank ACETONE
 Liquid level at mark and container sealed ✓
 Density of blank (pa) .7847 g/ml
 Blank volume (Va) 250 ml
 Date and time of wt. 4-25-86 0800 Gross wt. 110752.9 mg
 Date and time of wt. 4-25-86 1400 Gross wt. 110752.9 mg
 Average gross wt. 110752.9 mg
 Tare wt. 110752.7 mg
 Weight of blank (ma) .2 mg

$$Ca = \frac{ma}{Va \cdot pa} = \frac{(.2)}{(250)(.7847)} = .00102 \text{ mg/g}$$

Note: In no case shall a blank residue greater than (0.01 mg/g) or 0.001% of the weight of blank used be subtracted from the sample weight.

Remarks: _____

Signature of analyst _____

Signature of reviewer _____

METHOD 5

PARTICULATE SAMPLE RECOVERY AND INTEGRITY SHEET

Plant: GEN SHALE Sample date: 4-22-86
 Sample location: KNOXVILLE Run no.: #1
 Sample recovery person: KARSTENS Recovery date: SAME
 Filter(s) no.: #4

MOISTURE

Impingers Silica gel
 Final volume (wt) 35 ml (gm) Final wt. 959.1 g
 Initial volume (wt) 0 ml (gm) Initial wt. 953.7 g
 Net volume (wt) 35 ml (gm) Net wt. 5.4 g
 Total moisture 40.4 g
 Color of silica gel 1/10 PINK
 Description of impinger water CLEAR

RECOVERED SAMPLE

Filter container no. RUN # 1 sealed ✓
 Description of particulate on filter DK GREY - LT CHARCOAL

Acetone rinse container no. RUN # 1 Liquid level marked ✓
 Acetone blank container no. BLK Liquid level marked ✓

Samples stored and locked _____

Remarks: _____

Date of laboratory custody _____

Laboratory personnel taking custody _____

Remarks: _____

METHOD 5 TRAIN ANALYTICAL PARTICULATE DATA

Plant GEN SHALE Run No. #1
 Sample location KNOXVILLE
 Relative humidity 20%
 Density of acetone (pa) 7847 g/ml

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	/	/
filter(s)	/	/

Acetone rinse container no. #5
 Acetone rinse volume (Vaw) 200 ml
 Acetone blank residue concentration (Ca) .00102 mg/g
 $W_a = Ca \cdot Vaw \cdot pa = (.00102)(200)(.7847) = .16$ mg
 Date and time of wt 4-25-86 0800 Gross wt 1003522 mg
 Date and time of wt 4-25-86 1400 Gross wt 1003522 mg
 Average gross wt 1003522 mg
 Tare wt 1002960 mg
 Less acetone blank wt (Wa) .2 mg
 Weight of particulate in acetone rinse 56.0 mg

Filter(s) container no. #4
 Date and time of wt 4-25-86 0800 Gross wt 251.9 mg
 Date and time of wt 4-25-86 1400 Gross wt 251.9 mg
 Average gross wt 251.9 mg
 Tare wt 164.6 mg
 Weight of particulate on filter(s) 87.3 mg
 Weight of particulate in acetone rinse 56.0 mg
 Total weight of particulate 143.3 mg

Note: In no case shall a blank residue greater than (.01 mg/g) or .001% of the weight of acetone used be subtracted from the sample weight.

Remarks: _____

Signature of analyst [Signature]

Signature of reviewer [Signature]

METHOD 5

PARTICULATE SAMPLE RECOVERY AND INTEGRITY SHEET

Plant: GEN SHALE Sample date: 4-22-86
Sample location: KNOXVILLE Run no.: #2
Sample recovery person: KALSTENS Recovery date: SAME
Filter(s) no.: #6

MOISTURE

Impingers		Silica gel	
Final volume (wt)	<u>43</u> ml (gm)	Final wt.	<u>958.2</u> g
Initial volume (wt)	<u>0</u> ml (gm)	Initial wt.	<u>958.1</u> g
Net volume (wt)	<u>43</u> ml (gm)	Net wt.	<u>6.1</u> g
Total moisture		<u>49.1</u> g	
Color of silica gel		<u>1/10 PINK</u>	
Description of impinger water		<u>CLEAR</u>	

RECOVERED SAMPLE

Filter container no. RUN H 2 sealed ✓
Description of particulate on filter LT CHARCOAL

Acetone rinse container no.	<u>RUN H 2</u>	Liquid level marked	<u>✓</u>
Acetone blank container no.	<u>BLK</u>	Liquid level marked	<u>✓</u>
Samples stored and locked _____			
Remarks: _____			

Date of laboratory custody _____
Laboratory personnel taking custody _____
Remarks: _____

METHOD 5 TRAIN ANALYTICAL PARTICULATE DATA

Plant GEN SHALE Run No. #2
 Sample location KNOXVILLE
 Relative humidity 20%
 Density of acetone (pa) .7847 g/ml

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse filter(s)	<u>✓</u>	<u>✓</u>

Acetone rinse container no. #7
 Acetone rinse volume (Vaw) 225 ml
 Acetone blank residue concentration (Ca) .0010 mg/g
 $W_a = Ca \cdot Vaw \cdot pa = (.00102) (225) (.7847) = .18$ mg
 Date and time of wt 4-25-86 0800 Gross wt 107137.2 mg
 Date and time of wt 4-25-86 1400 Gross wt 107137.2 mg
 Average gross wt 107137.2 mg
 Tare wt 107073.9 mg
 Less acetone blank wt (Wa) .2 mg
 Weight of particulate in acetone rinse 63.1 mg

Filter(s) container no. #6
 Date and time of wt 4-25-86 0800 Gross wt 271.9 mg
 Date and time of wt 4-25-86 1400 Gross wt 271.9 mg
 Average gross wt 271.9 mg
 Tare wt 167.9 mg
 Weight of particulate on filter(s) 104.0 mg
 Weight of particulate in acetone rinse 63.1 mg
 Total weight of particulate 167.1 mg

Note: In no case shall a blank residue greater than (.01 mg/g) or .001% of the weight of acetone used be subtracted from the sample weight.

Remarks: _____

Signature of analyst Eug A. Kasten

Signature of reviewer [Signature]

METHOD 5

PARTICULATE SAMPLE RECOVERY AND INTEGRITY SHEET

Plant: GEN SHALE Sample date: 4-22-86
 Sample location: KNOXVILLE Run no.: #3
 Sample recovery person: KAMSTENS Recovery date: SAME
 Filter(s) no.: #7

MOISTURE

Impingers	Silica gel
Final volume (wt) <u>50</u> ml (gm)	Final wt. <u>960.7</u> g
Initial volume (wt) <u>0</u> ml (gm)	Initial wt. <u>954.7</u> g
Net volume (wt) <u>50</u> ml (gm)	Net wt. <u>6.0</u> g
Total moisture <u>56.0</u> g	
Color of silica gel	<u>1/10 PINK</u>
Description of impinger water	<u>CLEAR</u>

RECOVERED SAMPLE

Filter container no. RUN #3 sealed ✓
 Description of particulate on filter CHARCOAL - WET

Acetone rinse container no. <u>RUN #3</u>	Liquid level marked <u>✓</u>
Acetone blank container no. <u>BLK</u>	Liquid level marked <u>✓</u>

Samples stored and locked _____
 Remarks: _____

Date of laboratory custody _____
 Laboratory personnel taking custody _____
 Remarks: _____

METHOD 5 TRAIN ANALYTICAL PARTICULATE DATA

Plant GEN SHALE Run No. #3
 Sample location KNOXVILLE
 Relative humidity 20%
 Density of acetone (ρ_a) .7842 g/ml

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse filter(s)	<u>✓</u>	<u>✓</u>

Acetone rinse container no. # 12

Acetone rinse volume (V_{aw}) 225 ml

Acetone blank residue concentration (C_a) .00102 mg/g

$W_a = C_a V_{aw} \rho_a = (.00102)(225)(.7842) = .18$ mg

Date and time of wt 4-25-86 0800 Gross wt 106243.6 mg

Date and time of wt 4-25-86 1400 Gross wt 106243.6 mg

Average gross wt 106243.6 mg

Tare wt 106175.9 mg

Less acetone blank wt (W_a) .2 mg

Weight of particulate in acetone rinse 67.5 mg

Filter(s) container no. # 7

Date and time of wt 4-25-86 0800 Gross wt 258.3 mg

Date and time of wt 4-25-86 1700 Gross wt 258.3 mg

Average gross wt 258.3 mg

Tare wt 161.6 mg

Weight of particulate on filter(s) 96.7 mg

Weight of particulate in acetone rinse 67.5 mg

Total weight of particulate 164.2 mg

Note: In no case shall a blank residue greater than (.01 mg/g) or .001% of the weight of acetone used be subtracted from the sample weight.

Remarks: _____

Signature of analyst Greg A. Karsten

Signature of reviewer [Signature]

CHAIN OF CUSTODY LOG

Plant GENERAL SHALE - KNOXVILLE

Lab Location BIRMINGHAM

SAMPLE RECOVERY

Run #	Date	Time	I.D. Number	Type	Recovered by
<u>1</u>	<u>4-22</u>	<u>9:30</u>	<u>RUN #1</u>	<u>FILTER + ACETONE</u>	<u>G KARSTENS, C TURNER</u>
<u>2</u>	<u>4-22</u>	<u>11:30</u>	<u>RUN #2</u>	<u>"</u>	<u>" "</u>
<u>3</u>	<u>4-22</u>	<u>1:30</u>	<u>RUN #3</u>	<u>"</u>	<u>" "</u>

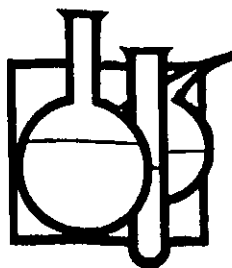
SAMPLE TRANSFER

From-Whom	To Whom	Date	Time
<u>NO TRANSFER</u>	<u>N/A</u>		

SAMPLE ANALYSIS

Container #	Method of Analysis	Date	Time	Analyst
<u>FILTER # 4 RUN1</u>	<u>DESSICATION + REWEIGH</u>	<u>4-25-86</u>	<u>0800, 1400</u>	<u>D Karstens</u>
<u># 6 RUN2</u>	<u>"</u>	<u>4-25-86</u>	<u>"</u>	<u>"</u>
<u># 7 RUN3</u>	<u>"</u>	<u>4-25-86</u>	<u>"</u>	<u>"</u>
<u>ACETONE # 5 RUN1</u>	<u>EVAPORATE + REWEIGH</u>	<u>4-25-86</u>	<u>"</u>	<u>"</u>
<u># 7 RUN2</u>	<u>"</u>	<u>4-25-86</u>	<u>"</u>	<u>"</u>
<u># 12 RUN3</u>	<u>"</u>	<u>4-25-86</u>	<u>"</u>	<u>"</u>

Approved by 



GUARDIAN SYSTEMS, INC.

305 Ashville Road
P.O. Box 300
Leeds, Alabama 35094
205/699-6647

April 30, 1986

Customer: General Shale Products Corp.
P.O. Box 3547, C.R.S.
Johnson City, TN 37601

Control number: 59591

Report to: Mr. Dave McNees

Sample date: 4/23/86

Sample Mark: Coal

Sample Number:

LABORATORY REPORT

<u>Parameter</u>	<u>Units</u>		<u>Results</u>
	<u>As Received</u>	<u>Dry Basis</u>	
Moisture, %	2.34		
Ash, %	4.21	4.31	
Sulfur, %	1.16	1.18	
Btu	13,707	14,035	
MAF, Btu		14,668	

Method Reference: "Standard Methods", 15th Ed., 1981
ASTM ANNUAL STANDARDS

Approved by: John Stithland

PROCESS INFORMATION

PLANT: KNOXVILLE 7B

DATE: APRIL 22, 1986

Brick Rate:

Car Schedule	=	<u>36</u>	Minutes	=	<u>1.67</u>	Cars/Hour
Car Count	=	<u>3,840</u>	S/S Brick/Car			
Hourly Rate	=	<u>6,400</u>	S/S Brick/Hour			
Brick Weight	=	<u>4.3</u>	Lbs.			
Brick Rate	=	<u>27,520</u>	Lbs./Hour			

Coal Rate:

Firing Rate	=	<u>14.89</u>	Tons Coal/Day
		<u>1,241</u>	Lbs. Coal/Hour
		<u>193.9</u>	Lbs. Coal/M Brick

Total Process Weight:

	<u>27,520</u>	Lbs. Brick/Hour
+	<u>1,241</u>	Lbs. Coal/Hour
	<u>28,761</u>	Total Lbs./Hour
	<u>14.38</u>	Tons/Hour *

Coal Analysis: (See Attached)

<u> </u>	Btu/Lb.	<u> </u>
<u> </u>	Sulfur	<u> </u>
<u> </u>	Ash	<u> </u>

Allowable Emissions:

* Based on input rate; 11.34 tons/hr. based on output (product) rate.

DAILY BURNING REPORT

PLANT 7 KILN B

DAY TUE. DATE 4-22-86

<u>COAL</u>	<u>BTU's</u>	<u>Therms</u>	<u>Cost</u>
<u>29,789 # @ 14000</u>	<u>= 41704740</u>	<u>= 4170 @ .176</u>	<u>= \$734.00</u>

Total Therms 4170 \$ 734.00 Total Cost

Total Brick Burned 153,600 \$ 4.77 Cost per M

Total Therms/M Brick Burned 27.1

SCHEDULE 36 min.

NO. CARS 40

TYPE BRICK 5/8 Antiques

~~XXXXXXXXXX~~

BTU's/# 754

U.C.T. 3.50

PREDRYER SUPPLY 140

KILOWATT HOURS 27164.16

POWER COST 1187.0

POWER COST PER M 5.29

PREDRYER COUNT _____

SUPERVISOR Charles Quinn

ANT: 7A and B

DAILY REPORT
KNOXVILLE, TENN.

Day Tuesday Date: 4-22-86

LOADING	STD	ACTUAL
nding Room Worked	16	16
nding Operated	15	11.6
s Per/Hour	55	59.2
eds Hauled	24	36
ens Modulus	2.5	-
marks:		
CHINING <i>Total 285.504</i>	8/Shift	1st 2nd 3rd
il Room Started		
ck Mach Norm- 20,000B/HR. <i>17733</i>		5.7 4.2 6.2
ck Machine Started		
orted Hacking Cored Brick		
pe ick Produced <i>5/5 Ft. Jordan</i>	1st 2nd 3rd	4.8 4.0 8.0
ck Hacked vs. Brick Made	%	%
cuum (Absolute)	2.5	2.2
sen strength	25	33
sen Brick Weight	4.4	4.3
lumn Temp.	100	98
id Area <i>27.0</i>	A: <i>28.0</i>	B: <i>27.7</i>
marks:		<i>22.6</i>
dryer		
sen ars	a b	a b
w i-Ent		
. Sup. Temp. <i>140</i>	<i>110</i>	<i>140</i>
marks:		
marks:		

BURNING	A	STD	B	A	ACTUAL	B
Kiln Schedule	65	36		65	36	
Cars Burned	22	40		21	40	
Car Count	3360	3840		3360	3840	
Brick Burned	78	145		70	153	
Type of Brick <i>5/5 Antiqua</i>						
Rate of Suction <i>0</i>	35			29	20	
Key Check Reading A&B	-	-		-	-	
Cold Water Absorption		6.0		5.7	5.6	
LOADING						
Brick Graded/Man Hour	2000				1913	
General Information						
No. Employees <i>104</i>		98			99	
N.U.B. Produced		12,000			6500	
Remarks:						
<i>BURNED brick wt.</i>				<i>3.35 lbs</i>		

FUEL REPORT

'A'	Nat. Gas	Cu. Ft.	Therm.	%
K	Fuel Oil	Gal.	Therm.	%
I	Coal <i>15,595</i>	Lb. <i>2185</i>	Therm.	%
L	Total Therms. Norm- <i>27.0</i>	<i>30.9</i>	Therms. Per.	
N	BTU/Lbs. Ware Norm-	<i>859</i>		
'B'	Nat. Gas	Cu. Ft.	Therm.	%
K	Fuel Oil	Gal.	Therm.	%
I	Coal <i>29,789</i>	Lb. <i>4170</i>	Therm.	%
L	Total Therms. Norm- <i>27.0</i>	<i>27.1</i>	Therm. Per.	
N	BTU/Lbs. Ware Norm-	<i>754</i>		

8,000 Berkley Iron Spat
Shape A - Hurstbourne

SUPERVISOR CADATE 4-22-86

GREEN BRICK AT 8:00 A.M.

KILN SCHEDULE 36 min.GREEN BRICK WEIGHT 5

STANDARD

PRODUCTION 153,600BURNED BRICK WEIGHT 3.6

SPECIAL

TYPE BRICK 56 AntiguosCARS BURNED 40

SOLID

TOTAL KILN HOURS

TOTAL BRICK BURNED

PAVER

KEY CHECK AVERAGE

TOTAL BRICK WEIGHT

OTHER

PUSHER PRESSURE 300TURBO PRESSURE 24.5

GAS PRESSURE

PREDRYER SUPPLY TEMP. 140

DRYER EXHAUST DRAFT

DRYER EXHAUST TEMP. 170

COLD AIR SUPPLY TEMP.

KILN EXHAUST DRAFT

UNDER CAR TEMP. 355

COAL SCREENING

COAL DRYER TEMP. 145

FLASHING SYSTEM

TURBO BLOWER (amps)

DRYER SUPPLY (amps)

DRYER EXHAUST (amps)

COLD AIR SUPPLY (amps)

KILN EXHAUST (amps)

IMP MILL (amps)

IMP MILL BLOWER (amps)

ENERGY METERS

END 370 635 4259

BEGIN 369 055 4129

TOTAL 1580 88.7 = 1308 207.36

GAS: c.f. 0.040 = 100,000

COAL: 29546 lb. (11000 = 4136 44.00) 4136 0.126 / therm = 728.01

FLASHING: 100,000

GAS: \$ per MCF, \$ per therm

TOTAL THERMS 4136

TOTAL THERMS PER M BRICK 26.9

KWHR PER M BRICK 26956.80 (6.0437)

KWHR COST PER M BRICK 1178.0 (5.17)

PREDRYER

WET BULB

DRY BULB

HUMIDITY

DEW POINT

BRICK BODY

FANS

DRYER

WET BULB

DRY BULB

HUMIDITY

DEW POINT

BRICK BODY

FANS

DRYER RECIRCULATING FANS

NO. 1

NO. 2

NO. 3

NO. 4

CONTROL VALVE PRESSURE

NO. 1 45%

NO. 2 5%

NO. 3 36%

NO. 4

COST THERM % OF TOTAL COST PER M THERMS PER M

COAL: \$ per ton, \$ per therm

BTU PER POUND OF BRICK 747

AVERAGE COST PER THERM

TOTAL COST 728.01

COST PER M BRICK 4.73

1 2 3 4

HOUR	CAR	TYPE	SCH
0800	11 28	11	904
0900	2 141		924
1000	3 165		1033
1100	2 146		1107
1200	2 134		1245
1300	4 105		1333
1400	3 124		1407
1500	4 89		1535

1600	3 61		435
1700	1 57		527
1800	0 134	123	616
1900	0 187		733
2000	0 114	116	807
2100	0 37	136	924
2200	0 20		1033
2300	0 26	108	1107

2400	2 22	29	1211
0100	5 14		133
0200	4 113		209
0300	6 50	143	321
0400	3 X		433
0500	4 100	39	507
0600	4 154	69	616
0700	2 37		733

1495
1490

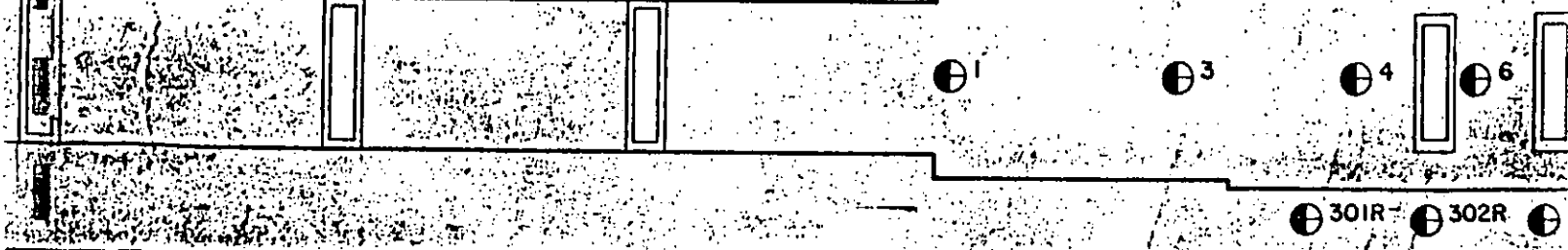
GENERAL SHALE PROCESSING PLANT

DRYER SUPPLY
202

KILN EXHAUST
201

301L 302L

REC NO. 2 REC NO. 3



5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20

DRYER KILN
SUPPLY EXH'T 700 EXHAUST
RECIRCULATING

Coal			202	201	1	3	301-R	301-L	4	302-R	302-L	6	303-R	303-L	7	304-R	304-L
TURBO		DRAFT															
24	145	48	340	565	710	810	905	895	850	880	920	960	1160	1125	1040	1210	1210
24	135	47	340	505	(720)	790	900	890	840	880	960	(955)	1140	1125	1045	1210	1210
24	140	46	340	515	(725)	820	920	895	(880)	880	970	(960)	1160	1130	1055	1220	1220
24	145	48	340	490	(720)	830	910	900	865	880	965	(970)	1165	1130	1045	1220	1220
24	145	46	340	515	(730)	830	915	905	(825)	880	970	(975)	1170	1130	1040	1230	1230
24	145	47	360	520	(730)	835	905	900	(720)	825	965	(970)	1165	1130	1040	1220	1220
24	140	46	345	500	(720)	810	910	900	(815)	870	965	(960)	1170	1130	1045	1225	1225
24	145	41	345	570	(715)	830	900	895	870	870	960	945	1105	1090	1040	1215	1215

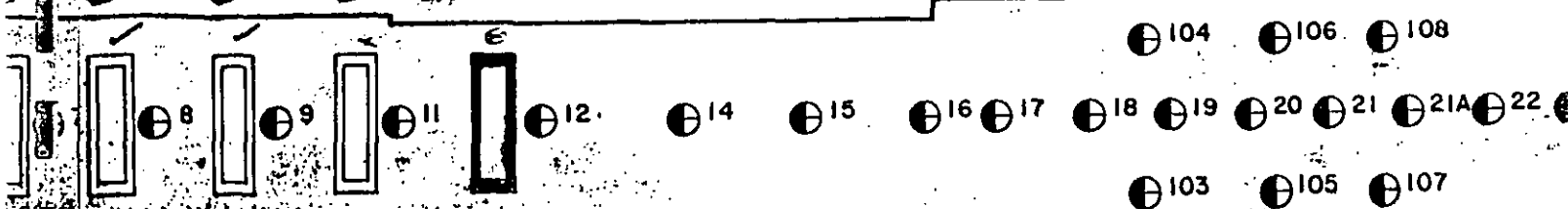
24	145	43	350	810	(615)	825	900	890	870	870	955	940	1105	1100	1040	1215	1215
24	145	44	350	870	(619)	830	900	895	870	870	960	940	1110	1105	1040	1220	1220
24	145	42	345	525	700	790	875	875	835	855	950	925	1075	1080	1040	1215	1215
45	140	42	350	525	700	790	880	880	835	855	950	930	1075	1085	1040	1210	1210
45	140	41	350	575	700	795	880	880	840	855	950	930	1080	1080	1040	1210	1210
31	140	41	340	505	(685)	790	865	860	870	855	940	920	1055	1060	1010	1195	1195
45	140	41	340	510	(685)	790	865	865	870	850	940	925	1060	1060	1010	1190	1190
45	145	41	340	510	675	785	855	855	825	840	935	910	1055	1060	1015	1205	1205

45	145	40	335	495	670	770	845	845	(865)	835	925	900	1040	1050	(990)	1190	1190
45	140	42	335	490	(660)	(765)	830	830	(800)	830	915	890	1035	1040	(980)	1180	1180
45	140	42	330	515	(655)	(660)	830	825	(790)	870	910	890	1030	1035	(975)	1180	1180
45	140	43	335	485	(650)	(760)	825	825	(805)	820	905	(880)	1020	1030	(990)	1175	1175
45	145	42	335	495	(660)	(755)	830	830	(800)	825	905	890	1025	1035	1000	1180	1180
45	145	42	330	505	(655)	(760)	830	830	(800)	835	915	885	1030	1040	1015	1180	1180
45	140	43	325	480	655	765	835	835	790	840	915	890	1030	1040	980	1190	1190
45	145	44	325	490	(655)	770	830	830	(805)	850	915	900	1040	1045	1005	1180	1180

PRODUCTS CORPORATION

TTN. 7B

303L 304L 305L 306L



304R 305R 306R

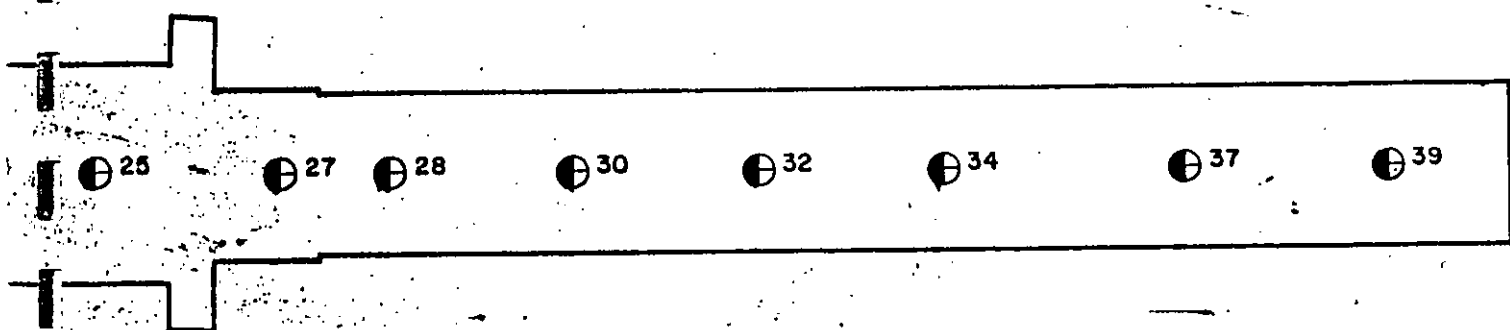
22 23 24 25 26 27 28 29 30 31 32 33 34 35 36 37

PREHEAT

12	2	1150	1350	1350	1330	1360	1360	1520	1580	1650	1670	1750	1790	1820	1820	1820	1860	1
304-L	8	305-R	305-L	9	306-R	306-L	11	12	14	15	16	17	18	103	104	19		
120	1155	1370	1350	1330	1350	1360	1500	1575	1650	1655	1730	1780	1825	1835	1810	1855	1	
120	1145	1370	1355	1325	1350	1365	1520	1600	1655	1660	1740	1785	1825	1835	1800	1865	1	
120	1155	1350	1365	1335	1365	1370	1515	1590	1665	1650	1730	1775	1825	1845	1710	1860	1	
120	1140	1375	1360	1330	1350	1360	1510	1590	1655	1665	1745	1780	1825	1825	1815	1865	1	
120	1155	1385	1360	1335	1355	1375	1530	1585	1665	1670	1750	1785	1825	1825	1810	1865	1	
120	1155	1370	1350	1350	1365	1380	1525	1590	1660	1670	1745	1790	1825	1820	1800	1855	1	
120	1155	1385	1365	1325	1355	1360	1510	1580	1655	1660	1735	1780	1825	1815	1815	1860	1	
240	1155	1375	1365	1340	1355	1360	1515	1580	1645	1660	1730	1775	1810	1810	1805	1865	1	

145	1160	1370	1370	1340	1355	1355	1515	1590	1655	1660	1730	1775	1820	1815	1810	1860	1
170	1160	1370	1370	1335	1360	1360	1525	1595	1660	1670	1735	1775	1810	1830	1815	1865	1
175	1160	1370	1380	1340	1355	1365	1540	1585	1655	1665	1730	1775	1815	1815	1810	1865	1
175	1160	1370	1380	1335	1350	1360	1540	1605	1655	1670	1735	1770	1815	1810	1800	1860	1
170	1160	1375	1350	1335	1356	1365	1530	1605	1670	1675	1735	1770	1815	1830	1800	1865	1
170	1145	1360	1355	1340	1360	1370	1520	1595	1675	1680	1740	1775	1810	1815	1805	1865	1
170	1145	1360	1380	1340	1365	1370	1520	1575	1640	1680	1745	1775	1810	1870	1805	1860	1
175	1145	1365	1355	1335	1360	1365	1520	1570	1640	1665	1740	1780	1810	1825	1810	1865	1

12	5	1136	1365	1356	1350	1365	1376	1500	1565	1630	1655	1730	1776	1820	1825	1825	1865	1
120	1115	1345	1340	1345	1365	1370	1485	1550	1625	1660	1730	1770	1810	1825	1810	1855	1	
195	1125	1340	1330	1340	1355	1365	1480	1550	1625	1650	1730	1775	1815	1825	1805	1865	1	
115	1095	1350	1335	1340	1356	1360	1500	1560	1630	1640	1735	1770	1810	1825	1810	1865	1	
195	1135	1355	1340	1335	1350	1360	1510	1565	1640	1645	1730	1760	1810	1790	1790	1850	1	
120	1140	1365	1350	1340	1360	1365	1510	1565	1640	1655	1725	1770	1820	1830	1815	1860	1	
125	1120	1370	1355	1340	1355	1360	1515	1565	1645	1660	1730	1770	1825	1830	1805	1860	1	
1200	1150	1380	1355	1335	1355	1360	1520	1565	1640	1655	1730	1770	1825	1825	1800	1865	1	



39	40	41	42	43	44	45	46	47	48	49	50	51	52	53
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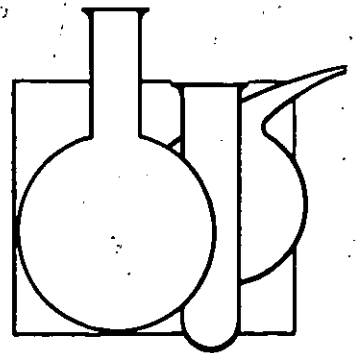
ZONE								COOLING							
106	21	107	108	21-A	22	23	24	25	27	28	30	32	34	37	39
1810	1860	1820	1820	1855	1810	1800	1750	1550	1300	1200	1100	900	700	100	100
1810	1860	1830	1805	1855	1775	1790	1745	1595	1325	1220	1030	905	665	95	115
1820	1860	1800	1820	1855	1775	1795	1740	1585	1320	1205	1040	910	645	100	115
1815	1860	1830	1820	1850	1780	1740	1735	1590	1310	1200	1030	920	655	110	130
1820	1860	1840	1810	1850	1775	1780	1740	1600	1325	1210	1040	930	665	105	125
1820	1855	1825	1830	1855	1780	1800	1735	1590	1315	1200	1020	910	645	105	125
1810	1855	1830	1825	1850	1775	1795	1735	1590	1325	1210	1015	910	655	105	145
1815	1860	1800	1800	1855	1780	1805	1750	1590	1320	1215	1030	905	650	110	130
1815	1860	1830	1835	1855	1780	1805	1745	1595	1325	1210	1035	895	650	105	125

FIREMAN															
1825	1855	1815	1815	1850	1780	1800	1740	1600	1320	1210	1040	890	650	105	125
1815	1860	1830	1815	1850	1785	1800	1740	1600	1320	1215	1045	890	650	105	120
1815	1865	1815	1810	1855	1780	1800	1740	1595	1325	1230	1030	915	650	105	125
1830	1860	1830	1830	1850	1785	1800	1740	1600	1325	1220	1030	915	655	105	125
1815	1865	1830	1830	1855	1785	1800	1740	1600	1320	1220	1030	910	655	105	120
1815	1860	1815	1815	1855	1785	1800	1740	1590	1330	1220	1035	915	665	100	120
1815	1860	1835	1815	1855	1785	1800	1740	1595	1330	1230	1000	915	660	100	120
1810	1865	1820	1810	1855	1780	1800	1740	1590	1325	1215	995	905	620	95	105

FIREMAN															
1830	1860	1835	1815	1855	1785	1800	1740	1600	1325	1215	1030	895	645	100	125
1830	1860	1830	1820	1855	1780	1795	1745	1605	1315	1200	1010	910	640	100	120
1840	1855	1835	1820	1855	1780	1800	1740	1595	1320	1205	1015	905	650	100	130
1835	1860	1835	1820	1850	1780	1795	1745	1595	1330	1225	1020	910	650	100	120
1825	1855	1815	1815	1855	1780	1795	1735	1600	1315	1210	1035	900	640	95	125
1825	1855	1805	1810	1850	1725	1790	1730	1590	1310	1200	1010	930	640	95	130
1830	1855	1830	1815	1855	1780	1790	1735	1600	1320	1190	1005	900	650	95	125
1820	1855	1815	1810	1850	1775	1790	1735	1595	1320	1190	990	890	640	95	115

FIREMAN

Calibrations



VI. METHOD 5 CALIBRATIONS

Meter Box

The meter box shall be initially calibrated every 6 months at the fixed settings of 0.5, 1.0, 1.5, 2.0, and 2.5 inches of water. Upon return to the laboratory from this test the meter box was be recalibrated using the average meter pressure for the test series. The recalibration point shall be the closest point to the initial calibration (for an average meter pressure of 0.92 a 1.00 "H₂O was used as the recalibration point). These recalibrations produced a single point MCF and a H@ which shall be compared to the original calibration to see if they are within the 5% allowed at the highest vacuum seen. These recalibration sheets are located behind the original calibration sheets.

Pitot Tubes

The S type tubes shall be calibrated against a standard pitot tube ($C_p = 0.99$) in a wind tunnel with a capacity to generate a test section velocity of approximately 3000 feet/ minute every 6 months. Additionally the pitot tube shall be measured as to its specifications and alignment. Upon return, the intercomponent spacings and the face opening alignment of the pitot tube assembly shall be rechecked and if no changes are noticed; it shall be assumed that the coefficient of the assembly had not changed.

Temperature measurements

All temperature devices (impinger, meter box, hot box and stack) shall be calibrated every 6 months against an ASTM mercury-in-glass reference thermometer or a reference thermocouple and potentiometer calibrated by fixed points, e.g., ice bath and boiling water (corrected to barometric pressure). Upon return the stack temperature device was recalibrated within 10% of the average absolute stack temperature. If the device being tested agrees within 1.5% of the reference device, the temperature data taken in the field shall be considered valid.

VL METHOD 5 CALIBRATIONS CONTINUED

Barometric Pressure

An aneroid barometer capable of measuring atmospheric pressure to within 0.1 inches Hg shall be used. If this device is defective the following alternate method shall be used. The barometric reading may be obtained from a nearby national weather service station, in which case the station value (which is the absolute barometric pressure) shall be requested and an adjustment for elevation differences between the weather station and sampling point shall be applied at a rate of minus 0.1 inches Hg per 100 feet elevation increase or vice versa for elevation decrease.

Specific Test equipment and measurements

The equipment used during these tests was as follows:

Probe: 5'-N

Meter Box: #700

Stack Temperature: OMEGA III

Sample Box: #2

Condenser: #1

The average temperature of the stack was 171° F. The OMEGA III was recalibrated at 170° F and agreed exactly with an ASTM mercury-in-glass reference thermometer. The intercomponent spacings and the face opening alignment of the Pitot Tube assembly was rechecked and no changes were noticed; therefore, it was assumed that the coefficient of the assembly had not changed.

Type A Glass Fiber Filters

FEATURES

- High tensile strength. ■ Excellent handling characteristics. ■ Good wetting properties. ■ Minimum of 99.9% retention for particles of $.3 \mu\text{m}$ as determined by DOP tests. ■ Binder free.

This is the original glass fiber filter pioneered by Gelman Instrument Company over 15 years ago. It continues to be widely used for high volume sampling. Since zinc is one of the raw materials incorporated in the glass fibers, Type A Filters have a variable zinc content. Another component of the filter, sulfuric acid, is used as a dispersion medium, making the sheets unsuitable for measurement of sulfates.

Type A Glass Fiber Filters are less likely to develop static charge or tear than other glass fiber media types. They are used extensively in applications where zinc and iron content is not important, or where sulfate content is not being determined.

Size	37 mm	47 mm	102 mm	8"x10"
Product No.	61715	61694	61696	61701
Filters/Pkg.	500	100	100	100

TYPE A GLASS FIBER FILTER SPECIFICATION REPORT

The following physical/chemical properties represent typical, average values obtained in accordance with accepted test methods. They are subject to normal manufacturing variations and are supplied as a technical service. The analysis has been made in accordance with EPA procedures (micrograms/8" x 10" sheet).

ELEMENTS:

Antimony	.30	Manganese	200
Arsenic	.30	Mercury	100
Beryllium	.1	Molybdenum	10
Bismuth	.10	Nickel	10
Cadmium	.5	Selenium	5000
Chromium	.10	Tin	10
Cobalt	.10	Titanium	170
Copper	.2	Vanadium	10
Iron	2300	Zinc	5000
Lead	.20		to 25,000

OTHER PHYSICALS:

BSO	.522	Flow Resistance (Max.)	
*pH	8.5	@ 320 cm/min.	.80 mm
DOP @320/cm/min		Flow Rate (air)	
(ASTM Method 2986) ..	99.9%	lpm/cm ² @ 70 cm Hg ..	50
Tensile Strength		Max. Use Temp.	400°C
(Fed. Spec. UUP31B) ..	750 gr	Static Properties	Low
Weight,		Ability to	
8"x10" sheet	4.0±.3 gr.	Fold	Excellent

WATER EXTRACTABLE IONS:

Sulfate	100	Chloride	1500
Nitrate	.50	Fluoride	.15
Ammonia	.20		

*pH—Gelman Procedure:

- 500 ml distilled water.
- Add 15 drops saturated KCl solution.
- Shred one 8"x10" sheet and soak in prepared water for one hour.
- Run pH at ambient temperature.

Type A/E Glass Fiber Filters

FEATURES

- Low trace metals. ■ Medium Handling characteristics. ■ Available in all sizes. ■ Minimum of 99.9% retention for particles of $.3 \mu\text{m}$ as determined by DOP tests. ■ Binder free.

Type A/E Glass Fiber Filters are composed of low acid soluble glass fiber. They contain low levels of both zinc and iron. The filters do react with atmospheric sulfur dioxide; and therefore, when high levels of sulfur are expected, corrections for this reaction should be accounted for.

Type A/E Glass Fiber Filters are binder free and ideal for gravimetric analysis of air pollutants. This pure, organic free filter is the basis for procedures widely used in determining municipal and industrial air polluting substances.

Size	25 mm	37 mm	47 mm	102 mm	8"x10"
Product No.	61630	61652	61631	61633	61638
Filters/Pkg.	500	500	100	100	100

TYPE A/E GLASS FIBER FILTER SPECIFICATION REPORT

The following physical/chemical properties represent typical, average values obtained in accordance with accepted test methods. They are subject to normal manufacturing variations and are supplied as a technical service. The analysis has been made in accordance with EPA procedures (micrograms/8" x 10" sheet).

ELEMENTS:

Antimony	.20	Manganese	.2
Arsenic	.20	Mercury	.80
Beryllium	.1	Molybdenum	.10
Bismuth	.10	Nickel	.10
Cadmium	.2	Selenium	.200
Chromium	.10	Tin	.10
Cobalt	.10	Titanium	.10
Copper	.2	Vanadium	.10
Iron	100-1800	Zinc	.90
Lead	.10		

OTHER PHYSICALS:

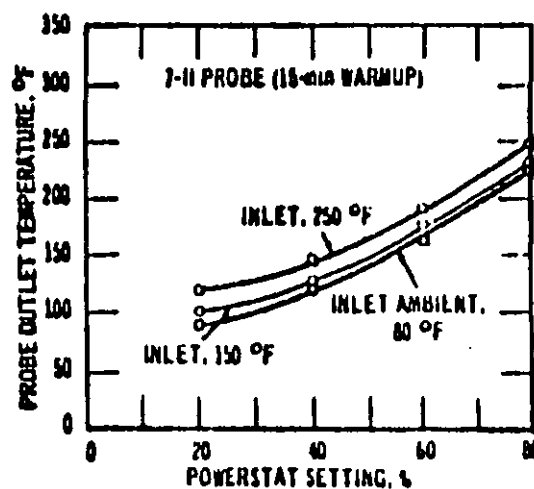
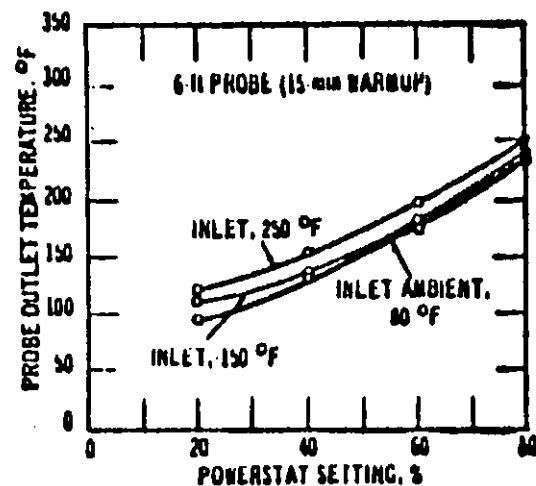
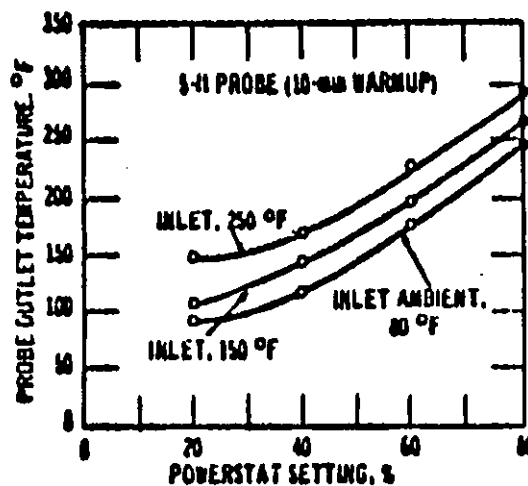
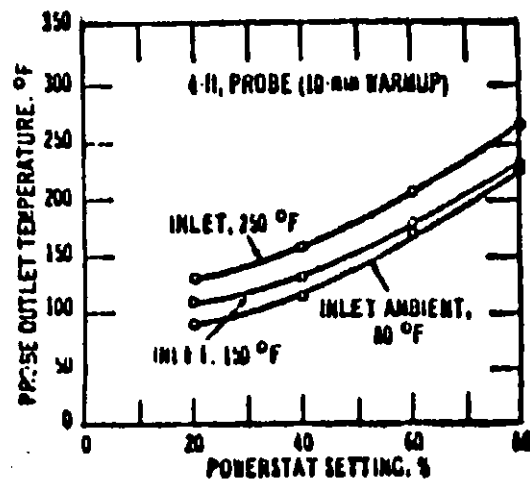
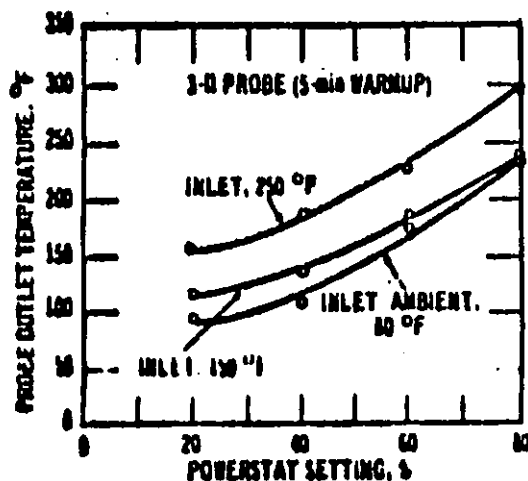
BSO	.522	Flow Resistance (Max.)	
*pH	9.0	@ 320 cm/min.	.80 mm
DOP @320/cm/min		Flow Rate (air)	
ASTM Methods 2986) ..	99.9%	lpm/cm ² @ 70 cm Hg ..	.60
Tensile Strength		Max. Use Temp.	400°C
(Fed. Spec. UUP31B) ..	600 gr.	Static Properties	Medium
Weight		Ability to	
8"x10" sheet	4.0±.3 gr.	Fold	Good

WATER EXTRACTABLE IONS:

Sulfate	.600	Chloride	.1500
Nitrate	.115	Fluoride	.87
Ammonia	.13		

*pH—Gelman Procedure:

- 500 ml distilled water.
- Add 15 drops saturated KCl solution.
- Shred one 8"x10" sheet and soak in prepared water for one hour.
- Run pH at ambient temperature.



NOTE: Flow rate held constant at 0.75; 50% change in flow rate has little effect on probe temperature.

GUARDIAN SYSTEMS INC
Initial Meter Calibration Box 700
on 4/07/86

Run Number	1	2	3	4	5
Barometric Pres, in Hg	30.10	30.10	30.10	30.10	30.10
Orifice pres drop, in H2O	0.5	1.0	1.5	2.0	2.5
Pres Wet Test Meter, in H2O	-0.42	-0.85	-1.11	-1.40	-1.70
Gas Volume Wet Init, CF	0.000	0.000	0.000	0.000	0.000
Gas Volume Wet Final, CF	6.056	8.883	10.532	12.430	13.986
Gas Volume Dry Init, CF	324.475	330.625	339.672	350.434	363.221
Gas Volume Dry Final, CF	330.625	339.672	350.434	363.221	377.682
Temp Wet Init, C	19.0	19.0	19.0	19.0	19.0
Temp Wet Final, C	19.0	19.0	19.0	19.0	18.8
Vapor Pressure, mm Hg	16.477	16.477	16.477	16.477	16.374
Dry Gas Temp Init In, F	92	91	95	97	99
Dry Gas Temp Final In, F	92	96	98	100	101
Dry Gas Temp Init Out, F	76	82	85	87	89
Dry Gas Temp Final Out, F	82	86	87	90	91
Run Time, sec	900	900	900	900	900
Meter Calibration Factor, Y	0.9966	0.9973	0.9967	0.9921	0.9883
Average Y	0.9942				
Qm	0.4037	0.5963	0.7083	0.8381	0.9442
Km	0.7270	0.7563	0.7325	0.7494	0.7546
Average Km	0.7440				
Delta HQ	1.74	1.61	1.72	1.64	1.62
Average HQ	1.66				

SIGNATURE G Karstens

GUARDIAN SYSTEMS INC
Recalibration of Meter Calibration Box 700
on 4/23/86

Run Number	1	2	3	Average
Barometric Pres, in Hg	30.15	30.15	30.15	30.15
Drifce pres drop, in H2O	1.0	1.0	1.0	1.0
Pres Wet Test Meter, in H2O	-0.76	-0.76	-0.76	-0.76
Gas Volume Wet Init, CF	0.000	0.000	0.000	0.000
Gas Volume Wet Final, CF	8.925	9.129	8.943	26.997
Gas Volume Dry Init, CF	707.503	716.675	726.149	2150.327
Gas Volume Dry Final, CF	716.675	726.149	735.503	2178.327
Temp Wet Init, C	16.5	17.0	17.2	16.9
Temp Wet Final, C	17.0	17.2	17.5	17.2
Vapor Pressure, mm Hg	14.303	14.622	14.856	14.594
Dry Gas Temp Init In, F	86	95	102	94.3
Dry Gas Temp Final In, F	95	104	105	101.3
Dry Gas Temp Init Out, F	78	82	92	84.0
Dry Gas Temp Final Out, F	82	92	93	89.0
Run Time, sec	900	930	900	2730
Meter Calibration Factor, Y	0.9928	0.9959	0.9955	0.9948
Qm	0.6012	0.6019	0.6147	0.6059
Km	0.7660	0.7619	0.7742	0.7673
Delta H _e	1.57	1.59	1.54	1.56
Previous Y	0.9973	% Difference	0.25	
Previous H _e	1.61	% Difference	2.83	

Project General Shore

Stack Knoxville

SIGNATURE

Lueg Karsten

TEMPERATURE CALIBRATION
FOR HOT BOX #2

DATE INITIAL 4-14-86

DATE FINAL

DEVICE READING (DEGREES F)

★ 220 230 240 250 260 270 280 ★

ACTUAL TEMPERATURE (DEGREES F)

11 11

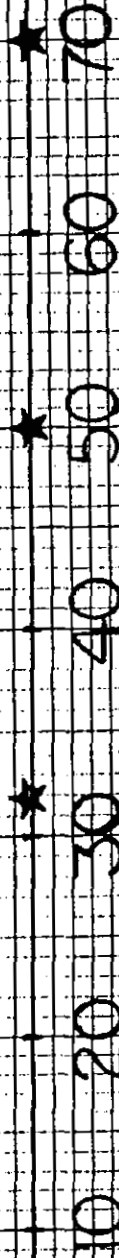
TEMPERATURE CALIBRATION

FOR IMPINGER #1

DATE INITIAL 4-14-86

DATE FINAL

DEVICE READING (DEGREES F)



ACTUAL TEMPERATURE (DEGREES F)

TEMPERATURE CALIBRATION

FOR OMEGA 3

FOR

DATE INITIAL DATE FINAL

4-11-96

DATE INITIAL

DEVICE READING (DEGREES F)

0 10 20 30 40 50 60 70 80

ACTUAL TEMPERATURE (DEGREES F)

111.1

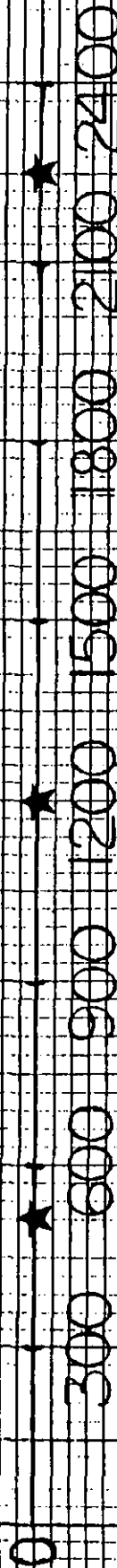
TEMPERATURE CALIBRATION

FOR OMEGA 3

DATE INITIAL 1-14-88

DATE FINAL

DEVICE READING (DEGREES F)



ACTUAL TEMPERATURE (DEGREES F)

PITOT CALIBRATION FORM

Date 3-7-86 Probe # 5'-N
 Calibrated By G. KARSTEN, C. TURNER
 Nozzle Size NA

SIDE A

Run #	ΔP_{std} (in. H ₂ O) Standard	$\Delta P(s)$ (in. H ₂ O) Type "s"	$C_p(s)$	Deviation $C_p(s) - \bar{C}_p(A)$
1	.335	.465	.840	+ .007
2	.34	.485	.829	- .004
3	.345	.49	.831	- .002
		$\bar{C}_p(A)$	.833	.83

SIDE B

Run #	ΔP_{std} (in. H ₂ O) Standard	$\Delta P(s)$ (in. H ₂ O) Type "s"	$C_p(s)$	Deviation $C_p(s) - \bar{C}_p(B)$
1	.335	.486	.822	- .008
2	.34	.48	.833	+ .003
3	.345	.485	.835	+ .005
		$\bar{C}_p(B)$	.830	.83

CALCULATIONS

$$C_p(s) = C_{p(std)} \sqrt{\frac{\Delta P_{std}}{\Delta P(s)}}$$

(or 0.99)

$$\text{Average Deviation} = \frac{\sum |C_p(s) - \bar{C}_p(A \text{ or } B)|}{3}$$

3

← Must be ≤ 0.01

$$|\bar{C}_p(A) - \bar{C}_p(B)| \leftarrow \text{Must be } \leq 0.01$$