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AIR POLLUTION EMISSION TEST

Marblehead Lime Company
(PLANT NAME)

Gary, Indiana
(PLANT ADDRESS)



U. S. ENVIRONMENTAL PROTECTION AGENCY
Office of Air and Water Programs
Office of Air Quality Planning and Standards
Emission Standards and Engineering Division
Emission Measurement Branch
Research Triangle Park, N. C. 27711



SOURCE SAMPLING

CONTRACT NO. 68-02-0238
TASK NO. 9

MARBLEHEAD LIME COMPANY
GARY, INDIANA
LIME KILN

Prepared for
Emissions Measurement Branch
Environmental Protection Agency

Prepared by
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(C-337-9)

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I. INTRODUCTION

Under the Clean Air Act, as amended, the Environmental Protection Agency is charged with the establishment of performance standards for new installations or modifications of existing installations in stationary source categories which may contribute significantly to air pollution. A performance standard is a standard for emissions of air pollutants which reflects the best emission reduction systems that have been adequately demonstrated (taking into account economic considerations).

The development of realistic performance standards requires accurate data on pollutant emissions within the various source categories. In the lime production industry, the No. 5 baghouse at Marblehead Lime Company, located in Gary, Indiana, was designated by EPA as representative of a well-controlled operation, and was thereby selected for the emission testing program. This report presents the results of the testing which was performed at the Gary facilities of Marblehead Lime during the week of June 10, 1974.

The tests performed were particulate, sulfur dioxide, nitrogen oxides, carbon monoxide, and visible emissions taken after the No. 5 baghouse serving No. 5 lime kiln at the Marblehead Lime Company, Gary, Indiana. The tests were conducted by Walden Research Division of Abcor Inc., under the technical direction of EPA Project Officer, John W. Brown. The process monitoring engineer was James Eddinger. The test crew consisted of Richard Furman, Program Manager for Walden, Lawrence Katzman, Gary Pulliam, David Jessich, and Denis Weder, Van Madden, Samuel Geer and Paul Wade from STW Testing, Inc., and Ralph Torborg from Honeywell Corporate Research. The tests included six four-hour runs designed to measure average emission rates.

II. SUMMARY AND DISCUSSION OF RESULTS

Tables 2-1 through 2-8 summarize the results of particulates, sulfur dioxide, nitrogen oxides, carbon monoxide, and visible emissions tests performed at the Marblehead Lime Company, Gary, Indiana. Tables 2-1, 2-3, and 2-5 give the test results in English units, while Tables 2-2, 2-4, and 2-6 give the results in Metric units.

The outlet particulate concentrations in Tables 2-1 and 2-2 are given for the front half (particulate matter collected on the filter and all sample-exposed surfaces prior to the filter) and the total particulate concentration including the condensible portion of the sample catch.

TABLE 2-1
PARTICULATE SUMMARY
ENGLISH UNITS

Proportion Rate

$\frac{1}{2} \times 37.76$

= 18.88

age
0.08
6.5
275
108
182
7.8
0.21
.20

Run Number	1	2	3
Date	June 11, 1974	June 12, 1974	
Volume of Gas Sampled-DSCF	181.62	162.69	163.91
Percent Moisture by Volume	6.5	4.8	6.3
Average Stack Temperature-°F	291	263	284
Stack Volumetric Flow Rate-DSCFM	23,797	22,407	23,162
Stack Volumetric Flow Rate-ACFM	37,049	33,031	35,532
Percent Isokinetic	98.5	93.7	91.4
Percent Stack Opacity	0.031	0.005	0.055
Feed Rate-ton/hr. (limestone only)	37.76	37.76	38.63

Particulates - Probe & Filter Catch

mg.	262.4	223.1	104.6	118.1	156.2	137.0	166.9
gr/DSCF	0.0223	0.0216	0.0098	0.0109	0.0125	0.0116	0.0148
gr/ACF	0.0143	0.0146	0.0064	0.0072	0.0082	0.0077	0.0097
lb/hr	4.55	4.15	1.96	1.98	2.67	2.30	2.92
lb/ton feed	0.1205	0.1099	0.0507	0.0513	0.0700	0.0602	0.0771

Particulates - Total Catch

mg.	424.5	426.0	340.0	275.0	320.4	377.0	360.5
gr/DSCF	0.0361	0.0404	0.0320	0.0254	0.0257	0.0319	0.0319
gr/ACF	0.0232	0.0274	0.0209	0.0167	0.0168	0.0210	0.0210
lb/hr	7.36	7.76	6.36	4.62	5.47	6.33	6.32
lb/ton feed	0.1949	0.2055	0.1646	0.1196	0.1432	0.1657	0.1656
Percent Impinger Catch	38.2	47.6	69.2	57.1	51.2	63.7	54.5

Multiply X 6
(see p. 5-1)

6 X 0.0771 = 0.4716/T



TABLE 2-2
PARTICULATE SUMMARY
METRIC UNITS

Run Number Date	1 June 11, 1974	2 June 11, 1974	3 June 12, 1974	4 June 12, 1974	5 June 13, 1974	6 June 13, 1974	Average
Volume of Gas Sampled-Nm ³	5.14	4.61	4.64	4.73	5.46	5.16	4.96
Percent Moisture by Volume	6.5	4.8	6.3	7.5	7.4	6.5	6.5
Average Stack Temperature-°C	143.9	128.3	140.0	131.7	133.3	133.9	135.2
Stack Volumetric Flow Rate-Nm ³ /min	674	635	656	602	705	656	655
Stack Volumetric Flow Rate-m ³ /min	1,049	935	1,006	917	1,077	993	996
Percent Isokinetic	98.5	93.7	91.4	101.6	100.0	101.6	97.8
Percent Stack Opacity	0.031	0.005	0.055	0.000	0.031	0.003	0.021
Feed Rate-M ton/hr (limestone only)	34.26	34.26	35.04	35.04	34.66	34.66	34.65
<u>Particulates - Probe & Filter Catch</u>							
mg.	262.4	223.1	104.6	118.1	156.2	137.0	166.9
mg/lm ³	51.1	48.4	22.5	25.0	28.6	26.6	33.7
mg/l ³	32.8	32.8	14.7	16.4	18.7	17.6	22.2
kg/hr	2.07	1.84	0.89	0.90	1.21	1.05	1.33
kg/11 ton	0.0604	0.0537	0.0254	0.0257	0.0349	0.0303	0.0384
<u>Particulates - Total Catch</u>							
mg.	424.5	426.0	340.0	275.0	320.4	377.0	360.5
mg/lm ³	82.6	92.4	73.3	58.1	58.7	73.1	73.0
mg/m ³	53.1	62.7	47.7	38.1	38.4	48.2	48.1
kg/hr	3.34	3.52	2.88	2.10	2.48	2.87	2.87
kg/11 ton	0.0975	0.1027	0.0822	0.0599	0.0715	0.0828	0.0828
Percent Impinger Catch	38.2	47.6	69.2	57.1	51.2	63.7	54.5

TABLE 2-3
SULFUR DIOXIDE SUMMARY
ENGLISH UNITS

Run Number Date	1		2		3		4		5		6		Average
	June 11, 1974		June 11, 1974		June 12, 1974		June 12, 1974		June 13, 1974		June 13, 1974		
Volume of Gas Sampled-DSCF	2.01	1.18	1.64	1.56	1.61	1.03	1.61	1.03	1.61	1.03	1.51	1.51	
Percent Moisture by Volume	6.5	4.8	6.3	7.5	7.4	6.5	7.4	6.5	7.4	6.5	6.5	6.5	
Average Stack Temperature-°F	291	263	284	269	272	273	272	273	272	273	275	275	
Stack Volumetric Flow Rate-DSCFM	23,797	22,407	23,162	21,247	24,878	23,156	24,878	23,156	24,878	23,156	23,108	23,108	
Stack Volumetric Flow Rate-ACFM	37,049	33,032	35,532	32,375	38,024	35,078	38,024	35,078	38,024	35,078	35,182	35,182	
<u>Laboratory Data</u>													
Normality of Barium Perchlorate-g-eq/l	0.0103	0.0103	0.0103	0.0103	0.0103	0.0103	0.0103	0.0103	0.0103	0.0103	0.0103	0.0103	
Titrant Volume Minus Blank													
Volume-mls													
Replicate 1	7.35	4.15	7.56	6.27	6.00	3.75	6.00	3.75	6.00	3.75			
Replicate 2	7.35	4.10	7.59	6.45	6.05	3.75	6.05	3.75	6.05	3.75			
Total Solution Volume-mls	100	100	100	100	121	117	121	117	121	117			
Volume of Sample Aliquot-mls	20	20	20	20	20	20	20	20	20	20			
<u>SO₂ Concentration - (Average of 2 Replicates</u>													
lbs/DSCF x 10 ⁻⁵	1.32	1.27	1.74	1.48	1.64	1.55	1.64	1.55	1.64	1.55	1.50	1.50	
ppm (Volume) @ 25°C	80.9	77.4	106	90.7	100	94.8	100	94.8	100	94.8	91.6	91.6	
lbs/hr	18.9	17.0	24.2	18.9	24.4	21.5	24.4	21.5	24.4	21.5	20.8	20.8	

TABLE 2-4

SULFUR DIOXIDE SUMMARY
METRIC UNITS

Run Number	1	2	3	4	5	6
Date	June 11, 1974	June 11, 1974	June 12, 1974	June 12, 1974	June 13, 1974	June 13, 1974
Volume of Gas Sampled-Nm ³	0.057	0.033	0.046	0.044	0.046	0.029
Percent Moisture by Volume	6.5	4.8	6.3	7.5	7.4	6.5
Average Stack Temperature-°C	143.9	128.3	140.0	131.7	133.3	133.9
Stack Volumetric Flow Rate-Nm ³ /min	674	635	656	602	705	656
Stack Volumetric Flow Rate-m ³ /min	1,049	935	1,006	917	1,077	993
Average						
Laboratory Data						
Normality of Barium Perchlorate-g-eq/l	0.0103	0.0103	0.0103	0.0103	0.0103	0.0103
Titration Volume Minus Blank Volume-mls						
Replicate 1	7.35	4.15	7.56	6.27	6.00	3.75
Replicate 2	7.35	4.10	7.59	6.45	6.05	3.75
Total Solution Volume-mls	100	100	100	100	121	117
Volume of Sample Aliquot-mls	20	20	20	20	20	20
SO ₂ Concentration - (Average of Replicates)						
gms/Nm ³	0.21	0.20	0.28	0.24	0.26	0.24
kg/hr	8.6	7.7	11.0	8.6	11.1	9.5
ppm	80.9	77.4	106	90.7	100	94.8
						91.6

TABLE 2-5
NITROGEN OXIDES SUMMARY
ENGLISH UNITS

Run Number	1	2	3	4	5	6	7	8	9	10	11	12	Average
Date	June 11, 1974	June 11, 1974	June 11, 1974	June 11, 1974	June 11, 1974	June 12, 1974	June 12, 1974	June 12, 1974	June 13, 1974	June 13, 1974	June 13, 1974	June 13, 1974	
Percent Moisture by Volume	6.5	6.5	6.5	6.5	6.3	6.3	6.3	6.3	7.4	7.4	7.4	7.4	6.7
Stack Volumetric Flow Rate-DSCFM	23,797	23,797	23,797	23,797	23,162	23,162	23,162	23,162	24,878	24,878	24,878	24,878	23,946
Stack Volumetric Flow Rate-ACFM	37,049	37,049	37,049	37,049	35,532	35,532	35,532	35,532	38,024	38,024	38,024	38,024	36,868
<u>Analysis</u>													
Flask Volume-mls	2,038	2,030	1,961	1,992	1,964	2,046	2,009	2,020	2,030	1,992	2,040	1,994	
Absorbant Volume-mls	26.0	24.5	24.0	25.5	25.0	25.0	25.0	24.0	26.0	26.0	25.0	26.0	
Initial Pressure-in. Hg.	1.89	1.89	1.79	1.89	2.04	1.81	1.80	1.78	1.62	1.59	1.62	1.68	
Final Pressure-in. Hg.	29.41	28.51	28.61	29.41	29.68	29.06	29.18	28.88	29.67	29.57	29.47	29.37	
Initial Temperature-°F	72.0	70.0	73.0	72.0	72.0	75.0	76.0	71.0	77.0	78.0	82.0	80.0	
Final Temperature-°F	76.0	74.0	73.0	74.0	80.0	81.0	81.0	82.0	85.0	85.0	86.0	83.0	
Total NO _x Collected-µg	145.6	132.0	138.8	146.7	143.1	143.1	118.1	107.4	279.1	221.9	268.4	225.5	
<u>NO_x Concentration</u>													
lbs/DSCF x 10 ⁻⁷ (as NO ₂)	49.4	46.2	29.9	50.7	50.5	49.2	41.2	37.7	94.8	77.0	91.5	78.7	59.7
ppm	42.1	39.4	42.5	43.2	43.0	41.9	35.1	32.1	80.8	65.6	77.9	67.0	50.9
lbs/hr.	7.05	6.60	7.12	7.24	7.02	6.84	5.73	5.24	14.2	11.5	13.7	11.7	8.66

TABLE 2-6

NITROGEN OXIDES SUMMARY
METRIC UNITS

Run Number	1	2	3	4	5	6	7	8	9	10	11	12	Average
Date	June 11, 1974	June 11, 1974	June 11, 1974	June 11, 1974	June 11, 1974	June 12, 1974	June 12, 1974	June 12, 1974	June 12, 1974	June 13, 1974	June 13, 1974	June 13, 1974	
Percent Moisture by Volume	6.5	6.5	6.5	6.5	6.3	6.3	6.3	6.3	7.4	7.4	7.4	7.4	6.7
Stack Volumetric Flow Rate-Nm ³ /min	674	674	674	674	656	656	656	656	705	705	705	705	678
Stack Volumetric Flow Rate-m ³ /min	1,049	1,049	1,049	1,049	1,006	1,006	1,006	1,006	1,077	1,077	1,077	1,077	1,044
<u>Analysis</u>													
Flask Volume-mls	2,038	2,030	1,961	1,992	1,964	2,046	2,009	2,020	2,030	1,992	2,040	1,994	
Absorbant Volume-mls	26.0	24.5	24.0	25.5	25.0	25.0	25.0	24.0	26.0	26.0	25.0	26.0	
Initial Pressure-mm Hg.	48.0	48.0	45.5	48.0	51.8	56.0	45.7	45.2	41.1	40.4	41.1	42.7	
Final Pressure-mm Hg.	747.0	724.2	726.7	747.0	753.9	738.2	741.2	733.6	753.6	751.1	748.6	746.0	
Initial Temperature-°C	22.2	21.1	22.8	22.2	22.2	23.9	24.4	21.7	25.0	25.6	27.8	26.7	
Final Temperature-°C	24.4	23.3	22.8	23.3	26.7	27.2	27.2	27.8	29.4	29.4	30.0	28.3	
Total NOx collected-µg	145.6	132.0	138.8	146.7	143.1	143.1	118.1	107.4	279.1	221.9	268.4	225.5	
<u>NOx Concentration</u>													
mg/Nm ³	79.1	74.0	79.9	81.2	80.9	78.8	65.0	60.4	151.9	123.3	146.6	126.1	95.7
ppm	42.1	39.4	42.5	43.2	43.0	41.9	35.1	32.1	80.8	65.6	77.9	67.0	50.9
kg/hr	3.20	2.99	3.23	3.28	3.18	3.10	2.60	2.38	6.44	5.22	6.21	5.31	3.93

TABLE 2-7
CARBON MONOXIDE SUMMARY
(INTEGRATED 2-HOUR BAG SAMPLES)

Date	Time	CO, ppm
June 11, 1974	1500 - 1700	15
June 12, 1974	1030 - 1230	580
June 13, 1974	930 - 1130	30

T.M. RUNS		AUG. DSCFM
1 23,797	2 22,407	1: 23,102
3 23,162	4 21,247	2: 22,205
5 24,878	6 23,156	3: 24,017

TABLE 2-8

Stack No. Date	1		2		3		4		5		6	
	June 11, 1974 Obs. 1 Obs. 2	June 11, 1974 Obs. 1 Obs. 2	June 11, 1974 Obs. 1 Obs. 2	June 11, 1974 Obs. 1 Obs. 2	June 12, 1974 Obs. 1 Obs. 2	June 12, 1974 Obs. 1 Obs. 2	June 12, 1974 Obs. 1 Obs. 2	June 12, 1974 Obs. 1 Obs. 2	June 13, 1974 Obs. 1 Obs. 2	June 13, 1974 Obs. 1 Obs. 2	June 13, 1974 Obs. 1 Obs. 2	June 13, 1974 Obs. 1 Obs. 2
Start Time	1238	1601	1556	1601	1053	1053	1342	1305	931	1146	1210	
Duration of Observation (min)	240	240	240	240	234	240	240	240	240	240	227	
Total No. of Readings	960	960	960	960	936	960	960	960	960	960	908	
No. Readings Unobservable	0	0	0	0	0	0	0	0	0	0	0	
No. Readings 0% Opacity	952	960	958	960	928	954	960	960	956	959	908	
5	6	0	2	0	7	4	0	0	2	1	0	
10	2	0	0	0	0	2	0	0	2	0	0	
15	0	0	0	0	2	0	0	0	0	0	0	
20-100	0	0	0	0	0	0	0	0	0	0	0	
Percent Readings Unobservable	0	0	0	0	0	0	0	0	0	0	0	
Percent Readings 0% Opacity	99.2	100.2	99.8	100.0	99.1	99.4	100.0	100.0	99.6	99.9	100.0	
5	0.6	0.0	0.2	0.0	0.7	0.4	0.0	0.0	0.2	0.1	0.0	
10	0.2	0.0	0.0	0.0	0.2	0.2	0.0	0.0	0.2	0.0	0.0	
15	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
20-100	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
Average Opacity =	0.062	0.000	0.010	0.000	0.069	0.042	0.000	0.000	0.031	0.005	0.000	
Sum of Nos.												
No. Readings Unobservable												

III. PROCESS DESCRIPTION AND OPERATION

Limestone consists primarily of calcium carbonate or combinations of calcium and magnesium carbonate with varying amounts of impurities. The most abundant of all sedimentary rocks, limestone is found in a variety of consistencies from marble to chalk. Lime is a calcined or burned form of limestone, commonly divided into two basic products — quicklime and hydrated lime. Calcination expels carbon dioxide from the raw limestone, leaving calcium oxide (quicklime). With the addition of water, calcium hydroxide (hydrated lime) is formed.

The basic processes in production are: (1) quarrying the limestone raw material; (2) preparing the limestone for kilns by crushing and sizing; (3) calcining the feed; and (4) optionally processing the quicklime further by additional crushing and sizing and the hydration. The majority of lime is produced in rotary kilns which can be fired by coal, oil, or gas. Rotary kilns have the advantages of high production per man-hour and a uniform product, but require higher capital investment and have higher unit fuel costs than most vertical kilns.

The Marblehead Lime plant has five rotary lime kilns operating on high calcium limestone. The product is a high calcium metallurgical lime which is used in the steel industry.

The No. 5 lime kiln, which was source tested by EPA, is 300 feet in length with an inside diameter of 10 feet 6 inches. The kiln has a design capacity of 500 tons per day. The limestone feed is brought into the plant sized to one and three-quarters by one-half inch. There is no stone pre-heater. The kiln is fired with pulverized coal.

The No. 5 lime kiln is provided with a baghouse manufactured by the Marblehead Lime Company. The exit gas from the lime kiln is cooled to about 500°F with a combination of water spray and tempering air. The cooled gases pass to a knock-out box where some chips and stones are removed and then to the induced draft fan. From the fan, the exhaust gas goes directly to the

TABLE 3-1

SUMMARY OF LIME KILN PROCESS
DATA DURING SAMPLING

Test Run	Date 1974	Limestone* Feed Rate tph	Fuel (coal)* Feed Rate tph	[REDACTED]	Baghouse Temp °F	Oxygen %
1, 2	June 11	37.76	5.77	1.7-2.0	570-592	[REDACTED]
3, 4	June 12	38.63	5.80	1.2-1.6	550-600	[REDACTED]
5, 6	June 13	38.21	5.58 5.71	1.4-1.5	560-600	[REDACTED]

* Feed rates were determined from the feed weight indicator during each test. A monitor of the process uniformity was obtained from feed rate meters, however, these meter readings were not calibrated to indicate the actual feed rates. These numbers are shown in Appendix F.

<u>FEED</u>	<u>PRODUCTION</u>
37.76	18.9
38.63	19.3
38.21	19.1

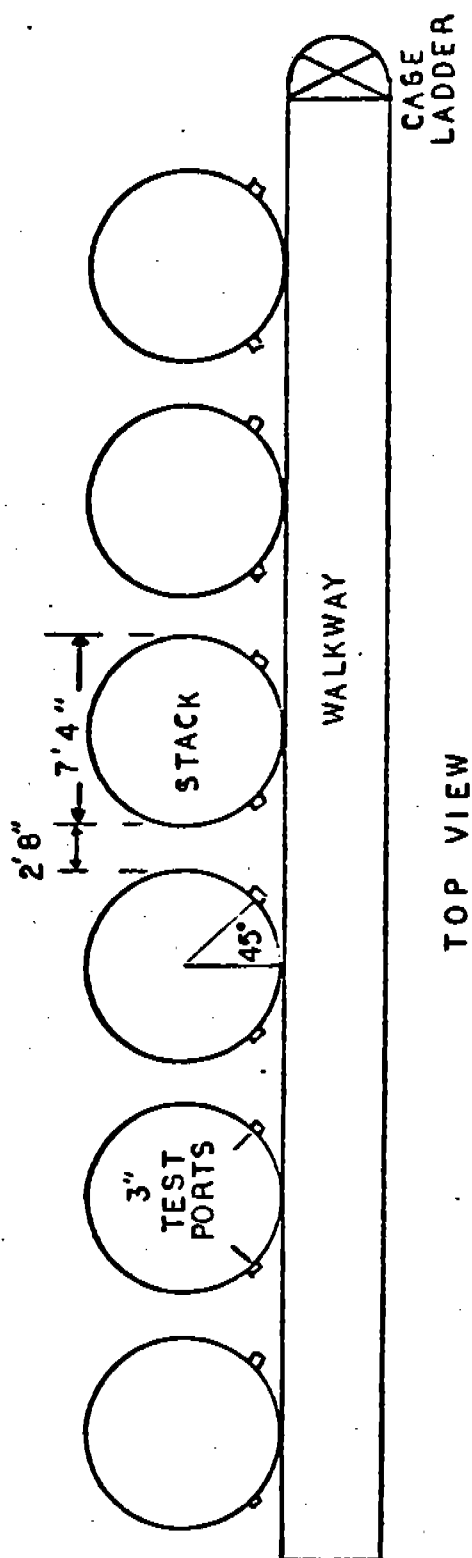
baghouse. This baghouse has twelve compartments, six stacks, and about 80,000 square feet of bag surface area. The bags are cleaned by reversing the air flow in a section. Each section is cleaned in sequence with a typical cleaning cycle taking about two hours. The dust collected is used by a portland cement manufacturer located nearby.

During testing, the baghouse stacks were sampled for particulates, SO₂, CO, and NO_x. Simultaneous visible emissions data were also recorded.

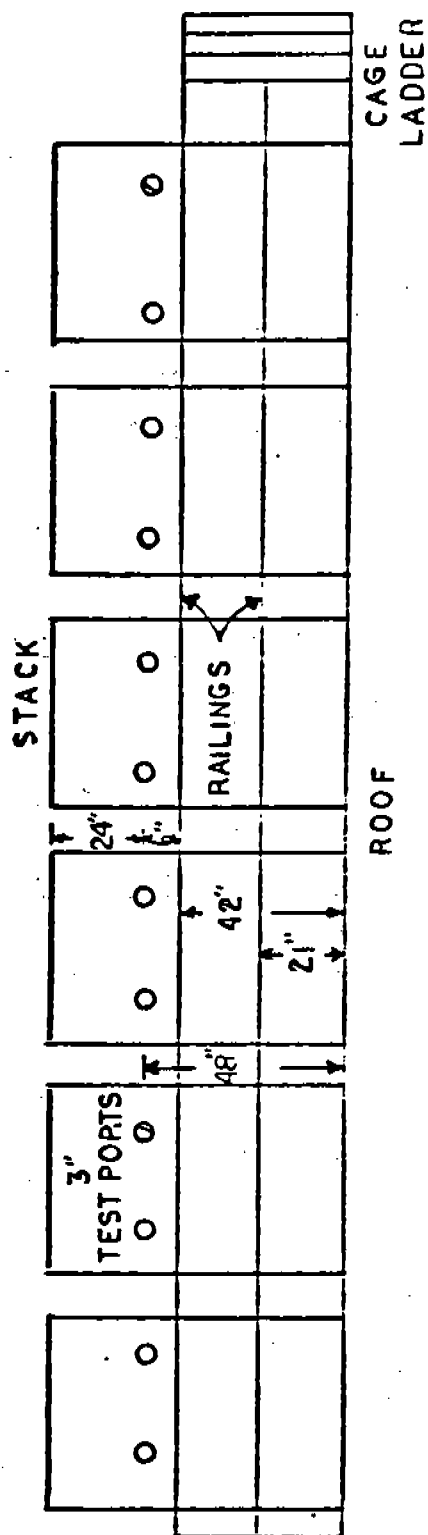
The operation of the kiln and the baghouse was monitored during the test and the process data recorded. Readings were taken about every half hour. These records are in Appendix F. As far as known from the process data and conversations with the operators, the kiln and baghouse operated normally during the tests. The main process information is summarized in Table 3-1.

IV. LOCATION OF SAMPLING POINTS

A schematic layout of the test location is shown in Figure 4-1. There are two three-inch sampling ports on each of the six stacks. They are located 90° apart, two feet from the outlet and six feet from the inlet. The stacks are 7'4" in diameter and therefore, require the maximum number of traverse points (48). Samples were taken at each of the 48 points for five minutes per point, or a total of 240 minutes (four hours) for each run.



TOP VIEW



SIDE VIEW

Figure 4-1. Test Location

V. SAMPLING AND ANALYTICAL PROCEDURES

All field sampling data is provided in Appendix F. All sample calculations and test results are provided in Appendices A through E.

A. PARTICULATE SAMPLING (EPA METHOD 5)

One four-hour particulate run was made on each of the six stacks and two particulate trains were used simultaneously. The particulate sampling was performed in accordance with EPA Method 5, Federal Register, December 23, 1971. The location of the sampling site, determination of stack gas velocity and volumetric flow rate, gas analysis for carbon dioxide and dry molecular weight, and determination of moisture in the stack gases were performed in accordance with Methods 1, 2, 3, and 4, respectively, of the aforementioned document.

The variations from Method 5 as described in the Federal Register were the addition of one hundred milliliters of water to the third impinger and the use of a stationary impinger box connected to the heated filter box through Teflon tubing. Normally, the third impinger is left empty, however, the addition of water did not alter the sampling methods or results as the water was eventually evaporated in a beaker for the determination of particulate matter in the residual water fraction. Approval was granted by the EPA Project Officer for use of the stationary impinger box, Teflon tubing, and stainless steel probe. The sampling train is shown in Figure 5-1.

Due to the low velocities (about 15 feet per second), inclined manometers with a range of 0 - 0.25 inches H₂O were used. Nomographs were not used for the adjustment of the sampling rate, rather the equations that serve as the basis for the nomograph were calculated. A direct relationship between the stack velocity head (ΔP_s) and the pressure differential across the orifice meter (ΔH) was determined and used for setting the isokinetic sampling rate. The relationship is as follows:

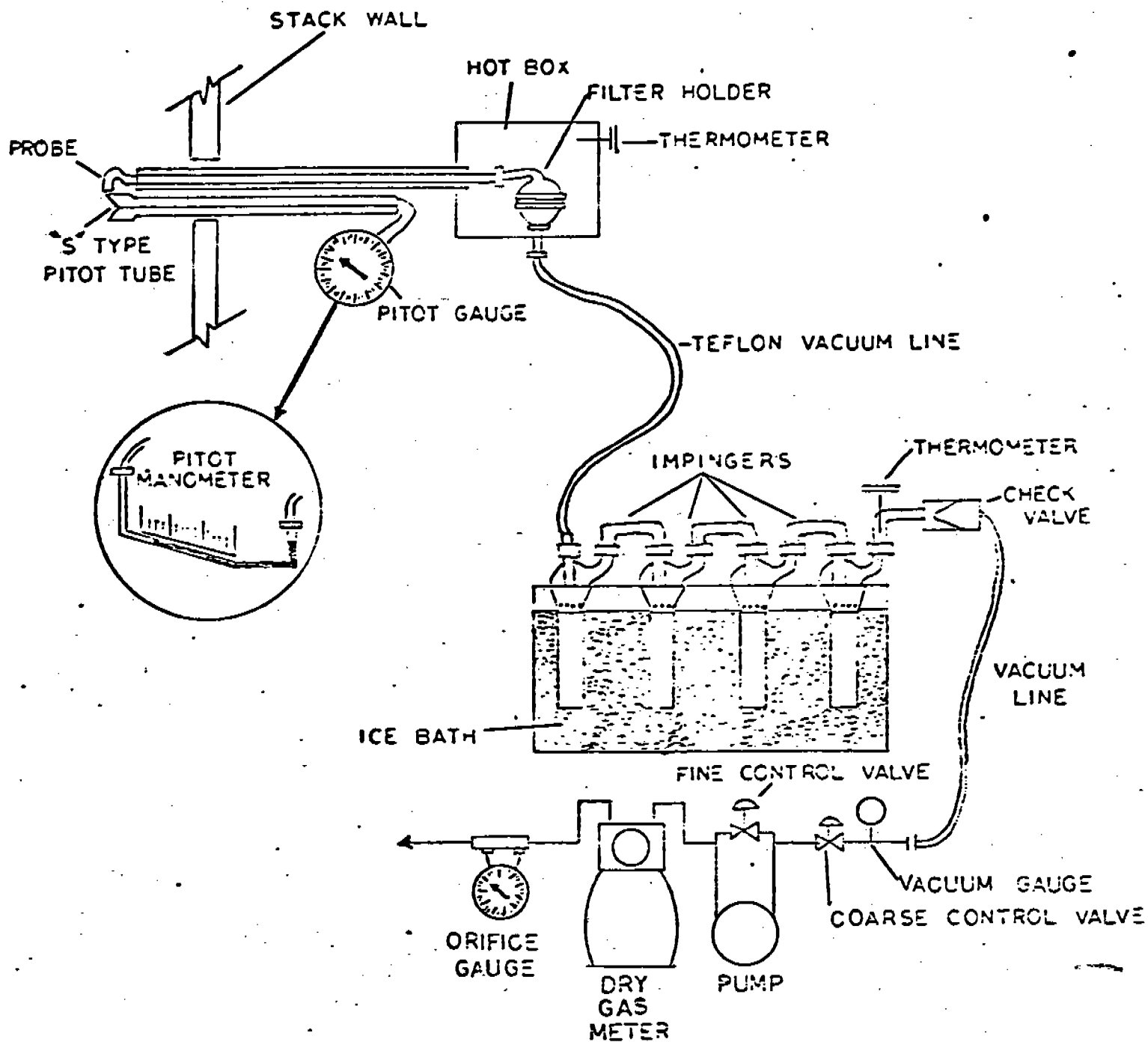


Figure 5-1. Particulate Sampling Train, Marblehead Lime, Gary, Indiana

$$\left[\frac{(2.9) \left(\frac{\text{STD}}{\text{P.C.F.}} \right) (60) (\pi) (D)^2 (1-B) (T_m)}{4(144) (T_s)^{1/2} (\text{O.C.F.})} \right]^2 \Delta P = \Delta H$$

where:

STD P.C.F. = Pitot correction factor (dimensionless)
 D = Diameter of nozzle, inches
 B = Percent moisture in gas stream
 T_m = Meter temperature, °R
 T_s = Stack temperature, °R
 O.C.F. = Orifice correction factor

Also, a meter rate formula was determined and used to maintain isokinetic flow by checking the flow rate at 15-second intervals. We have found this approach to be quite accurate as the two equations serve as a check for each other. The meter rate formula is as follows:

$$M_r = (\text{P.C.F.}) \times V_{\text{avg.}} \times 60 \times \frac{T_m}{T_s} \times \frac{P_b \pm P_s}{P_b - P_m} \times A_n \times (1 - \%H_2O)$$

where:

M_r = Volumetric flow rate, ft³/min.
 P.C.F. = Pitot correction factor (dimensionless)
 V_{avg.} = Average velocity, ft/sec
 T_m = Meter temperature, °R
 T_s = Stack temperature, °R
 P_b = Barometric pressure, in. Hg.
 P_s = Stack static pressure, in. Hg.
 P_m = Vacuum at meter, in. Hg.
 A_n = Area of nozzle, ft²
 %H₂O = Percent moisture in gas stream

The stack gas molecular weight was determined by three 4-hour integrated gas analyses collected simultaneously with the particulate tests. An Orsat was used to determine CO₂ and Fyrites were used to determine CO₂ and O₂. The Orsat scale is only capable of reading up to 21%. Since the O₂ is read together with the CO₂, a reading above 21% (16.5% O₂ and 7.0% CO₂ = 23.5% total) was obtained and therefore, Fyrites were used.

Sample recovery and analysis were performed in accordance with the methods described in the Federal Register, August 17, 1971. At the request of the Project Officer, a front-half water wash was performed after the acetone wash. This procedure should be used when testing lime kilns due to the nature of the particulate emissions. All sample bottles were acid-washed Wheaton bottles in accordance with specifications requested by the EPA. The tared beakers and filters containing the particulate matter will be held by EPA for their use.

B. SULFUR DIOXIDE (METHOD 6)

Six sulfur dioxide tests were performed in accordance with EPA Method 6, Federal Register, December 23, 1971. The probe was located in various stacks so there would be no interference with the traversing particulate sampling train. The tests were not run for the complete 4-hour period due to carry-over of the sulfuric acid fraction in the isopropanol impinger. Each test was conducted until bubbles from the first isopropanol impinger began carrying over into the second impinger containing the sulfur dioxide fraction. Two replicate analyses were performed by the barium thorin titration method on each sample and recorded as the average of the two replicates.

C. NITROGEN OXIDES (METHOD 7)

The nitrogen oxide tests were performed in accordance with EPA Method 7, Federal Register, December 23, 1971, and a modified draft supplied by the EPA. Four NO_x flasks were taken for each of the three days during the particulate tests. The samples were analyzed colorimetrically using the phenoldisulfonic acid procedure at the Walden laboratories.

D. CARBON MONOXIDE (METHOD 10)

Three 2-hour integrated bag samples were collected during the particulate tests. The carbon monoxide was measured according to Method 10 in the Federal Register, March 8, 1974. Carbon monoxide tests were conducted by Honeywell Corporate Research using a Honeywell NDIR Analyzer. Although CO , CO_2 and CH_4 channels were available, only the CO channel was operated.

EPA Method 10 specifies that for both integrated (bag) and continuous sampling, the sample must pass through a volume of silica gel and another of ascarite immersed in an ice bath (to remove H₂O and CO₂). Tests with the Honeywell NDIR CO Analyzer have demonstrated rejection ratios greater than 10⁴ for both H₂O and CO₂. Therefore, passing the sample through silica gel and ascarite is unnecessary. In fact, passing the sample through the ascarite caused considerable technical difficulty. After about an hour of sampling, the ascarite formed a hard ball around the inlet tube to the ascarite container, causing a severe flow restriction.

E. VISIBLE EMISSIONS (METHOD 9)

The relative opacity of each of the six stacks was determined in accordance with Method 9 of the Federal Register, December 23, 1971. The opacity determinations were conducted for two hours on each stack during the particulate tests. Two observers read each stack except Stack No. 5, which was read by one observer.

APPENDIX A
PARTICULATE TEST RESULTS
AND SAMPLE CALCULATION

WALDEN SOURCE TEST REPORT

COMPANY= MARBLEHEAD LIME COMPANY

PLANT= LIME KILN NUMBER 5

LOCATION= GARY, INDIANA

PROCESS= LIME KILN

CONTROL EQUIPMENT= BAGHOUSE

TEST SCHEDULE

RUN NO. DATE POLLUTANTS SAMPLED

1	11JUN 74	PART	SO2	NOX	CO	OPACITY
2	11JUN 74	PART	SO2			OPACITY
3	12JUN 74	PART	SO2	NOX	CO	OPACITY
4	12JUN 74	PART	SO2			OPACITY
5	13JUN 74	PART	SO2	NOX	CO	OPACITY
6	13JUN 74	PART	SO2			OPACITY

MARBLEHE

FIELD TEST DATA SUMMARY TEST NO. 1

PROBE LOCATION= STACK NO.1

COLLECTOR TYPE= EPA TRAIN

AMBIENT TEMPERATURE= 67.0 DEGREES FAHRENHEIT

BAROMETRIC PRESSURE= 29.10 INCHES MERCURY

PROBE LENGTH= 13.0 FEET

NOZZLE DIAMETER= 0.50 INCHES

PITOT TUBE CALIBRATION FACTOR= 0.83

STACK AREA= 42.24 SQ. FT.

GAS ANALYSIS

CO2 = 6.8 %

CO = 0.0 %

O2 = 19.5 %

N2 = 73.7 %

MOLECULAR WEIGHT= 29.87 • DRY BASIS

EXCESS AIR= **** %

SPECIAL INFORMATION (ALL 6 PARTICULATE TEST RUNS)

The outlet of the baghouse consists of six stacks. Each stack is 7.3 feet in diameter. One particulate run was made on each of the stacks. The meter temperatures given to the computer were set at 70°F because the Joy control unit that was used corrects the meter volume for temperature. No values for pump vacuum were taken and therefore 0.0 is shown. 300 ml. of water was used in the impingers (100 ml. in each of the first three impingers).

MARBLEHE

TRAVERSE SUMMARY (TEST NO. 1)

POINT NO.	CLOCK TIME	METER VOLUME	PITOT DELTAP	TUBE ONIFICE DELTAP	STACK TEMP.	METER INLET	TEMPERATURE OUTLET	PUMP VACUUM	IMPINGER TEMP.
	(MIN)	(GAL)	(IN. H ₂ O)	(IN. H ₂ O)	(DEG F)	(DEG F)	(DEG F)	(IN. HG)	(DEG F)
START	1225	357.280							
N24	30	360.900	0.04	0.70	275.0	70.0	70.0	0.0	60.0
N23	35	364.600	0.04	0.70	275.0	70.0	70.0	0.0	60.0
N22	40	0.0	0.04	0.80	300.0	70.0	70.0	0.0	60.0
N21	45	372.100	0.06	1.00	300.0	70.0	70.0	0.0	60.0
N20	50	375.900	0.04	0.90	300.0	70.0	70.0	0.0	60.0
N19	55	379.700	0.04	0.90	300.0	70.0	70.0	0.0	60.0
N18	1300	0.0	0.05	1.00	300.0	70.0	70.0	0.0	60.0
N17	5	388.100	0.05	1.00	300.0	70.0	70.0	0.0	60.0
N16	10	392.800	0.05	0.90	300.0	70.0	70.0	0.0	60.0
N15	15	397.100	0.05	0.90	300.0	70.0	70.0	0.0	60.0
N14	20	0.0	0.05	1.00	300.0	70.0	70.0	0.0	60.0
N13	25	404.700	0.05	1.00	300.0	70.0	70.0	0.0	60.0
N12	30	408.600	0.05	1.00	290.0	70.0	70.0	0.0	60.0
N11	35	412.500	0.05	1.00	300.0	70.0	70.0	0.0	65.0
N10	40	416.500	0.05	1.00	300.0	70.0	70.0	0.0	60.0
N 9	45	420.200	0.04	0.90	290.0	70.0	70.0	0.0	65.0
N 8	50	423.800	0.05	1.00	290.0	70.0	70.0	0.0	65.0
N 7	55	427.600	0.05	1.00	290.0	70.0	70.0	0.0	65.0
N 6	1400	431.400	0.05	1.00	280.0	70.0	70.0	0.0	65.0
N 5	5	435.200	0.05	1.00	275.0	70.0	70.0	0.0	65.0
N 4	10	439.100	0.05	1.00	275.0	70.0	70.0	0.0	65.0
N 3	15	443.000	0.05	1.00	260.0	70.0	70.0	0.0	65.0
N 2	20	446.800	0.05	1.00	260.0	70.0	70.0	0.0	65.0
N 1	25	450.420	0.04	0.90	240.0	70.0	70.0	0.0	65.0
S24	1605	454.000	0.04	0.80	285.0	70.0	70.0	0.0	50.0
S23	10	457.500	0.04	0.80	285.0	70.0	70.0	0.0	50.0
S22	15	461.000	0.04	0.80	290.0	70.0	70.0	0.0	50.0
S21	20	465.000	0.05	0.90	290.0	70.0	70.0	0.0	50.0

MARBLEHE

TRAVERSE SUMMARY (CONTINUED)

POINT NO.	CLOCK TIME	METER VOLUME	PITOT TUBE DELTAP	ORIFICE DELTAP	STACK TEMP.	METER TEMPERATURE INLET	TEMPERATURE OUTLET	PUMP VACUUM	IMPIGNER TEMP.
	(MIN)	(GAL)	(IN. H ₂ O)	(IN. H ₂ O)	(DEG F)	(DEG F)	(DEG F)	(IN. HG)	(DEG F)
S20	25	468.700	0.05	0.90	290.0	70.0	70.0	0.0	60.0
S19	30	472.600	0.05	0.90	290.0	70.0	70.0	0.0	60.0
S18	35	476.500	0.05	1.10	300.0	70.0	70.0	0.0	60.0
S17	40	480.500	0.05	1.10	300.0	70.0	70.0	0.0	70.0
S16	45	484.500	0.05	1.10	300.0	70.0	70.0	0.0	75.0
S15	50	488.500	0.05	1.10	300.0	70.0	70.0	0.0	75.0
S14	55	492.500	0.05	1.10	300.0	70.0	70.0	0.0	75.0
S13	1700	496.500	0.05	1.10	300.0	70.0	70.0	0.0	80.0
S12	5	500.800	0.06	1.20	295.0	70.0	70.0	0.0	80.0
S11	10	504.800	0.06	1.20	300.0	70.0	70.0	0.0	80.0
S10	15	509.200	0.06	1.20	300.0	70.0	70.0	0.0	80.0
S9	20	513.200	0.05	1.10	300.0	70.0	70.0	0.0	80.0
S8	25	517.100	0.05	1.10	300.0	70.0	70.0	0.0	80.0
S7	30	521.000	0.05	1.10	295.0	70.0	70.0	0.0	70.0
S6	35	525.000	0.05	1.10	300.0	70.0	70.0	0.0	65.0
S5	40	529.000	0.05	1.15	300.0	70.0	70.0	0.0	60.0
S4	45	533.000	0.05	1.10	300.0	70.0	70.0	0.0	60.0
S3	50	537.000	0.05	1.10	300.0	70.0	70.0	0.0	60.0
S2	55	540.500	0.04	1.00	270.0	70.0	70.0	0.0	60.0
S1	1800	543.590	0.03	0.65	260.0	70.0	70.0	0.0	60.0
AVERAGE OF 48 POINTS			0.05	0.99	290.6	70.0	70.0	0.0	64.2

MARBLEHE

PARTICULATE TEST SUMMARY-RUN NO. 1

STACK DATA

AVERAGE VELOCITY HEAD= 0.22
ACTUAL VELOCITY= 14.6 FEET PER SECOND (FPS)
PERCENT ISOKINETIC FLOW= 98.5 %
MOISTURE CONTENT= 6.5 %
MOLECULAR WEIGHT, WET BASIS= 29.10
VOLUMETRIC FLOW= 1427802.0 SCFH, DRY
2222941.0 ACFM
37049.0 ACFM ✓

LABORATORY DATA

(Front Half Only)

FILTER CATCH = 78.5 MG.
FRONT HALF (ACETONE WASH) = 113.3 MG.
FRONT HALF (WATER WASH) = 70.6 MG.
BACK HALF (ACETONE WASH) = 19.2 MG.
BACK HALF (ORGANIC EXTRACT) = 4.2 MG.
BACK HALF (WATER RESIDUE) = 138.7 MG.
TOTAL PARTICULATE COLLECTED = 424.5 MG.

78.5 MG.
113.3 MG.
70.6 MG.
262.4 MG.

TEST RESULTS-PARTICULATE EMISSIONS

GRAINS/SCF, DRY= 3.61E-02
POUNDS/SCF, DRY= 5.15E-06
POUNDS/HOUR= 7.36E 00
POUNDS/1000 POUNDS FLUE GAS= 7.33E-02

$$262.4 \text{ mg} : 4.55 \frac{\text{lb}}{\text{hr}} = 57.67 \frac{\text{mg}}{\text{lb}}$$

ORGANIC = $57.67 \frac{\text{mg}}{\text{lb}} \times 9.2 \text{ mg} = 530.2 \text{ mg}$
~~57.67 mg~~ $1 \frac{\text{lb}}{\text{hr}} = 0.728 \frac{\text{lb}}{\text{hr}}$
 $4.2 \text{ mg} \times 57.67 \text{ mg} = 242.3 \text{ mg}$

INORGANIC : $(19.2 + 138.7) \text{ mg} \times \frac{1 \text{ lb}}{\text{hr}} = 157.9 \text{ mg}$
 $= 2.74 \frac{\text{lb}}{\text{hr}}$

MARBLEHE

FIELD TEST DATA SUMMARY TEST NO. 2

PROBE LOCATION= STACK NO.2

COLLECTOR TYPE= EPA TRAIN

AMBIENT TEMPERATURE= 67.0 DEGREES FAHRENHEIT

BAROMETRIC PRESSURE= 29.10 INCHES MERCURY

PROBE LENGTH= 13.0 FEET

NOZZLE DIAMETER= 0.50 INCHES

PITOT TUBE CALIBRATION FACTOR= 0.83

STACK AREA= 42.24 SQ. FT.

GAS ANALYSIS

CO2= 6.8 %

CO = 0.0 %

O2 = 19.5 %

N2 = 73.7 %

MOLECULAR WEIGHT= 29.87 , DRY BASIS

*EXCESS AIR= **** %

SPECIAL INFORMATION (TEST #2 ONLY)

~~THIS TEST-RUN, THE HEATED PITOT TUBE CAUSED THE PROBE TO BE DAMAGED.~~

MARBLEHE

TRAVERSE SUMMARY (TEST NO. 2)

POINT NO.	CLOCK TIME	METER VOLUME (GAL)	PITOT TUBE DELTAP (IN. H ₂ O)	ORIFICE DELTAP (IN. H ₂ O)	STACK TEMP. (DEG. F)	METER INLET TEMP. (DEG. F)	METER OUTLET TEMP. (DEG. F)	PUMP VACUUM (IN. HG)	IMPINGING TEMP. (DEG. F)
START	1226	435.510							
N 1	31	439.600	0.05	0.75	270.0	70.0	70.0	0.0	55.0
N 2	36	443.400	0.05	0.81	270.0	70.0	70.0	0.0	55.0
N 3	41	447.400	0.05	0.92	275.0	70.0	70.0	0.0	55.0
N 4	46	451.300	0.05	0.92	275.0	70.0	70.0	0.0	55.0
N 5	51	455.100	0.05	0.90	270.0	70.0	70.0	0.0	55.0
N 6	56	459.900	0.05	0.92	275.0	70.0	70.0	0.0	55.0
N 7	1301	462.000	0.05	0.95	270.0	70.0	70.0	0.0	55.0
N 8	6	466.000	0.05	0.98	255.0	70.0	70.0	0.0	50.0
N 9	36	470.100	0.05	1.00	275.0	70.0	70.0	0.0	55.0
N 10	41	474.000	0.05	0.98	280.0	70.0	70.0	0.0	55.0
N 11	46	477.900	0.05	0.98	280.0	70.0	70.0	0.0	55.0
N 12	51	481.000	0.03	0.77	275.0	70.0	70.0	0.0	55.0
N 13	56	484.700	0.03	0.73	260.0	70.0	70.0	0.0	55.0
N 14	1401	487.800	0.03	0.60	260.0	70.0	70.0	0.0	55.0
N 15	6	490.900	0.04	0.65	270.0	70.0	70.0	0.0	60.0
N 16	11	494.200	0.04	0.69	265.0	70.0	70.0	0.0	60.0
N 17	16	498.000	0.04	0.78	265.0	70.0	70.0	0.0	55.0
N 18	21	501.500	0.04	0.75	260.0	70.0	70.0	0.0	55.0
N 19	26	505.000	0.04	0.80	260.0	70.0	70.0	0.0	55.0
N 20	31	508.100	0.03	0.55	255.0	70.0	70.0	0.0	55.0
N 21	36	511.100	0.03	0.58	255.0	70.0	70.0	0.0	55.0
N 22	41	514.300	0.04	0.65	250.0	70.0	70.0	0.0	55.0
N 23	46	518.800	0.04	0.88	250.0	70.0	70.0	0.0	55.0
N 24	51	521.520	0.04	0.85	250.0	70.0	70.0	0.0	55.0
S 1	1606	524.300	0.03	0.52	260.0	70.0	70.0	0.0	50.0
S 2	11	527.700	0.03	0.52	260.0	70.0	70.0	0.0	50.0
S 3	16	530.000	0.04	0.60	260.0	70.0	70.0	0.0	50.0
S 4	21	533.700	0.03	0.58	260.0	70.0	70.0	0.0	55.0

MARBLEHE

TRAVERSE SUMMARY (CONTINUED)

POINT NO.	CLOCK TIME (MIN)	METER VOLUME (ACF)	PITOT TUBE DELTAP (IN. H2O)	ORIFICE DELTAP (IN. H2O)	STACK TEMP. (DEG F)	METER INLET (DEG F)	TEMPERATURE OUTLET (DEG F)	PUMP VACUUM (IN. HG)	IMPINGER TEMP. (DEG F)
S 5	26	536.800	0.03	0.62	250.0	70.0	70.0	0.0	50.0
S 6	31	540.500	0.05	1.00	260.0	70.0	70.0	0.0	55.0
S 7	36	544.900	0.03	0.68	260.0	70.0	70.0	0.0	60.0
S 8	41	547.700	0.05	0.98	270.0	70.0	70.0	0.0	60.0
S 9	46	551.600	0.05	0.98	260.0	70.0	70.0	0.0	65.0
S10	51	555.200	0.04	0.90	270.0	70.0	70.0	0.0	65.0
S11	56	558.600	0.04	0.85	260.0	70.0	70.0	0.0	70.0
S12	1701	562.000	0.03	0.70	260.0	70.0	70.0	0.0	70.0
S13	6	565.300	0.04	0.78	260.0	70.0	70.0	0.0	65.0
S14	11	568.800	0.04	0.80	275.0	70.0	70.0	0.0	65.0
S15	16	572.200	0.04	0.80	260.0	70.0	70.0	0.0	70.0
S16	21	575.700	0.04	0.80	275.0	70.0	70.0	0.0	70.0
S17	26	579.600	0.05	1.02	275.0	70.0	70.0	0.0	70.0
S18	31	583.300	0.05	0.75	260.0	70.0	70.0	0.0	70.0
S19	36	586.700	0.04	0.73	250.0	70.0	70.0	0.0	60.0
S20	41	590.000	0.03	0.69	260.0	70.0	70.0	0.0	60.0
S21	46	593.200	0.03	0.68	270.0	70.0	70.0	0.0	60.0
S22	51	595.500	0.03	0.60	260.0	70.0	70.0	0.0	60.0
S23	56	599.200	0.03	0.63	260.0	70.0	70.0	0.0	60.0
S24	1801	602.420	0.04	0.75	240.0	70.0	70.0	0.0	60.0
AVERAGE OF 48 POINTS			0.04	0.78	263.4	70.0	70.0	0.0	58.2

MARBLEHE

PARTICULATE TEST SUMMARY-RUN NO. 2

SLACK DATA

AVERAGE VELOCITY HEAD= 0.20
 ACTUAL VELOCITY= 13.0 FEET PER SECOND (FPS)
 PERCENT ISOKINETIC FLOW= 93.7 %
 MOISTURE CONTENT= 4.8 %
 MOLECULAR WEIGHT, WET BASIS= 29.30
 VOLUMETRIC FLOW= 1344402.0 SCFH, DRY
 1981892.0 ACFH
 33031.5 ACFM

LABORATORY DATA

(Front Half Only)

FILTER CATCH = 92.5 MG.
 FRONT HALF (ACETONE WASH) = 83.4 MG.
 FRONT HALF (WATER WASH) = 47.2 MG.
 BACK HALF (ACETONE WASH) = 15.6 MG.
 BACK HALF (ORGANIC EXTRACT) = 3.5 MG.
 BACK HALF (WATER RESIDUE) = 183.8 MG.
 TOTAL PARTICULATE COLLECTED = 426.0 MG.

92.5 MG.
 83.4 MG.
 47.2 MG.
 223.1 MG.

Flow $\frac{1}{2}$: 223.1 mg : 4.15 $\frac{14}{hr}$ = 53.76 $\frac{mg}{(14/hr)}$

IES

(Front Half Only)

OPERATE 3.5 mg $\times \frac{14}{hr}$ = 0.651 $\frac{14}{hr}$

2.16E-02
 3.02E-06
 4.06E-00
 4.27E-02

INORGANIC (15.6+183.8) mg $\times \frac{1}{(14/hr)}$ = 3.709

.15E-02

MARBLEHE

FIELD TEST DATA SUMMARY TEST NO. 3

PROBE LOCATION= STACK NO.3

COLLECTOR TYPE= EPA TRAIN

AMBIENT TEMPERATURE= 74.0 DEGREES FAHRENHEIT

BAROMETRIC PRESSURE= 29.21 INCHES MERCURY

PROBE LENGTH= 13.0 FEET

NOZZLE DIAMETER= 0.50 INCHES

PITOT TUBE CALIBRATION FACTOR= 0.83

STACK AREA= 42.24 SQ. FT.

GAS ANALYSIS

CO2= 7.0 %

CO = 0.0 %

O2 = 16.5 %

N2 = 76.5 %

MOLECULAR WEIGHT= 29.78 , DRY BASIS

EXCESS AIR= **** %

MARBLEHE

TRAVERSE SUMMARY (TEST NO. 3)

POINT NO.	CLOCK TIME	METER VOLUME	PITOT TUBE DELTAP	ORIFICE DELTAP	STACK TEMP.	METER INLET	TEMPERATURE OUTLET	PUMP VACUUM	IMPINGER TEMP.
	(MIN)	(ACE)	(IN. H ₂ O)	(IN. H ₂ O)	(DEG F)	(DEG F)	(DEG F)	(IN. HG)	(DEG F)
START	1030	602.590							
S24	35	606.300	0.04	0.85	270.0	70.0	70.0	0.0	60.0
S23	40	610.200	0.05	1.00	270.0	70.0	70.0	0.0	55.0
S22	45	613.800	0.04	0.85	270.0	70.0	70.0	0.0	55.0
S21	50	619.000	0.05	1.05	270.0	70.0	70.0	0.0	60.0
S20	55	622.300	0.05	1.10	270.0	70.0	70.0	0.0	60.0
S19	1100	626.400	0.05	1.10	285.0	70.0	70.0	0.0	60.0
S18	5	630.700	0.05	1.10	275.0	70.0	70.0	0.0	60.0
S17	10	634.800	0.05	1.10	270.0	70.0	70.0	0.0	60.0
S16	15	638.900	0.05	1.10	275.0	70.0	70.0	0.0	60.0
S15	20	643.000	0.05	1.10	285.0	70.0	70.0	0.0	60.0
S14	25	647.200	0.05	1.15	280.0	70.0	70.0	0.0	60.0
S13	30	651.400	0.05	1.10	280.0	70.0	70.0	0.0	60.0
S12	35	654.800	0.03	0.80	280.0	70.0	70.0	0.0	60.0
S11	40	658.400	0.04	0.90	280.0	70.0	70.0	0.0	65.0
S10	45	662.300	0.04	0.90	290.0	70.0	70.0	0.0	60.0
S9	50	665.500	0.03	0.75	295.0	70.0	70.0	0.0	60.0
S8	55	669.200	0.04	0.90	295.0	70.0	70.0	0.0	60.0
S7	1200	672.300	0.03	0.75	295.0	70.0	70.0	0.0	60.0
S6	5	675.400	0.03	0.75	275.0	70.0	70.0	0.0	60.0
S5	10	678.600	0.03	0.70	275.0	70.0	70.0	0.0	60.0
S4	15	681.800	0.03	0.65	255.0	70.0	70.0	0.0	60.0
S3	20	685.500	0.04	0.80	235.0	70.0	70.0	0.0	60.0
S2	25	689.200	0.04	0.80	180.0	70.0	70.0	0.0	55.0
S1	30	691.850	0.02	0.50	185.0	70.0	70.0	0.0	55.0
N24	1300	695.500	0.04	0.90	320.0	70.0	70.0	0.0	60.0
N23	5	699.200	0.04	0.90	320.0	70.0	70.0	0.0	60.0
N22	10	703.300	0.05	1.10	310.0	70.0	70.0	0.0	55.0
N21	15	707.800	0.06	1.20	310.0	70.0	70.0	0.0	60.0

MARBLEHE

TRAVERSE SUMMARY (CONTINUED)

POINT NO.	CLOCK TIME	METER VOLUME	PITOT TUBE DELTAP	ORIFICE DELTAP	STACK TEMP.	METER TEMPERATURE INLET	TEMPERATURE OUTLET	PUMP VACUUM	IMPINGER TEMP.
	(MIN)	(GAL)	(IN. H ₂ O)	(IN. H ₂ O)	(DEG F)	(DEG F)	(DEG F)	(IN. HG)	(DEG F)
N20	20	712.300	0.06	1.30	310.0	70.0	70.0	0.0	60.0
N19	25	716.400	0.05	1.10	300.0	70.0	70.0	0.0	60.0
N18	30	720.500	0.05	1.10	300.0	70.0	70.0	0.0	60.0
N17	35	725.000	0.06	1.30	305.0	70.0	70.0	0.0	60.0
N16	40	729.400	0.06	1.30	305.0	70.0	70.0	0.0	60.0
N15	45	734.000	0.06	1.30	300.0	70.0	70.0	0.0	60.0
N14	50	738.300	0.06	1.30	300.0	70.0	70.0	0.0	60.0
N13	55	742.800	0.06	1.40	300.0	70.0	70.0	0.0	60.0
N12	1400	746.800	0.05	1.20	295.0	70.0	70.0	0.0	60.0
N11	5	750.500	0.04	1.00	295.0	70.0	70.0	0.0	60.0
N10	10	754.200	0.04	0.90	290.0	70.0	70.0	0.0	60.0
N9	15	758.000	0.04	0.90	290.0	70.0	70.0	0.0	60.0
N8	20	762.300	0.05	1.10	290.0	70.0	70.0	0.0	60.0
N7	25	766.400	0.05	1.15	290.0	70.0	70.0	0.0	60.0
N6	30	770.600	0.05	1.20	275.0	70.0	70.0	0.0	65.0
N5	35	774.700	0.05	1.15	290.0	70.0	70.0	0.0	65.0
N4	40	778.800	0.05	1.15	300.0	70.0	70.0	0.0	65.0
N3	45	782.900	0.05	1.15	290.0	70.0	70.0	0.0	60.0
N2	50	787.200	0.05	1.15	300.0	70.0	70.0	0.0	60.0
N1	55	770.100	0.02	0.50	300.0	70.0	70.0	0.0	60.0
AVERAGE OF 48 POINTS			0.05	1.01	283.9	70.0	70.0	0.0	59.9

MARBLEHE

PARTICULATE TEST SUMMARY-RUN NO. 3

SIACK DATA

AVERAGE VELOCITY HEAD= 0.21
ACTUAL VELOCITY= 14.0 FEET PER SECOND (FPS)
PERCENT ISO KINETIC FLOW= 91.4 %
MOISTURE CONTENT= 6.3 %
MOLECULAR WEIGHT, WET BASIS= 29.04
VOLUMETRIC FLOW= 1389/31.0 SCFH, DRY
2131933.0 ACFH
35532.2 ACFM

LABORATORY DATA

(Front Half Only)

FILTER CATCH = 35.9 MG.
FRONT HALF (ACETONE WASH) = 51.7 MG.
FRONT HALF (WATER WASH) = 17.0 MG.
BACK HALF (ACETONE WASH)
BACK HALF (ORGANIC EXTRACT)
BACK HALF (WATER RESIDUE)
TOTAL PARTICULATE COLLECTED

FRONT 1/2 : 104.6 MG : 1.96 lb/hr = 53.37 $\frac{mg}{lb/hr}$

TEST RESULTS-PARTICULATE EMISSIONS
GRAINS/SCF, DRY= 3.20E-02
POUNDS/SCF, DRY= 4.57E-06
POUNDS/HOUR= 6.36E 00
POUNDS/1000 POUNDS FLUE GAS

(Front Half Only)
9.84E-03
1.41E-06
1.96E-00
2.00E-02

ORGANIC 3.4 mg * $\frac{1}{53.37} \frac{mg}{lb/hr}$ = 0.0637 $\frac{lb}{hr}$

INORGANIC (19.7 + 212.3) $\frac{mg}{lb/hr}$ * $\frac{1}{53.37} \frac{mg}{lb/hr}$

= 4.35 $\frac{lb}{hr}$

WARHLEHE

FIELD TEST DATA SUMMARY TEST NO. 4

PROBE LOCATION= STACK NO.4

COLLECTOR TYPE= EPA TRAIN

AMBIENT TEMPERATURE= 74.0 DEGREES FAHRENHEIT

BAROMETRIC PRESSURE= 29.21 INCHES MERCURY

PROBE LENGTH= 13.0 FEET

NOZZLE DIAMETER= 0.50 INCHES

PITOT TUBE CALIBRATION FACTOR= 0.83

STACK AREA= 42.24 SQ. FT.

GAS ANALYSIS

CO2= 7.0 %
CO = 0.0 %
O2 = 16.5 %
N2 = 76.5 %

MOLECULAR WEIGHT= 29.78, DRY BASIS

EXCESS AIR= *** %

MARBLEHE

TRAVERSE SUMMARY (TEST NO. 4)

POINT NO.	CLOCK TIME	METER VOLUME	PITOT TUBE DELTAP	ORIFICE DELTAP	STACK TEMP.	METER INLET	TEMPERATURE OUTLET	PUMP VACUUM	IMPINGER TEMP.
	(MIN)	(GAL)	(IN. H ₂ O)	(IN. H ₂ O)	(DEG F)	(DEG F)	(DEG F)	(IN. HG)	(DEG F)
START	1025	546.690							
N 1	30	550.500	0.02	0.45	260.0	70.0	70.0	0.0	60.0
N 2	35	553.400	0.03	0.53	260.0	70.0	70.0	0.0	55.0
N 3	40	556.200	0.03	0.53	255.0	70.0	70.0	0.0	55.0
N 4	45	559.400	0.03	0.70	260.0	70.0	70.0	0.0	55.0
N 5	50	562.600	0.03	0.70	260.0	70.0	70.0	0.0	55.0
N 6	55	565.800	0.03	0.70	260.0	70.0	70.0	0.0	60.0
N 7	1105	693.300	0.04	0.83	265.0	70.0	70.0	0.0	60.0
N 8	5	572.800	0.04	0.85	270.0	70.0	70.0	0.0	60.0
N 9	10	576.900	0.04	0.93	260.0	70.0	70.0	0.0	60.0
N 10	15	580.000	0.04	0.87	260.0	70.0	70.0	0.0	60.0
N 11	20	583.900	0.05	1.18	265.0	70.0	70.0	0.0	60.0
N 12	25	587.900	0.05	1.08	270.0	70.0	70.0	0.0	60.0
N 13	30	591.200	0.03	0.72	265.0	70.0	70.0	0.0	60.0
N 14	35	594.100	0.03	0.57	280.0	70.0	70.0	0.0	60.0
N 15	40	597.300	0.03	0.72	280.0	70.0	70.0	0.0	60.0
N 16	45	600.600	0.04	0.85	280.0	70.0	70.0	0.0	60.0
N 17	50	604.000	0.03	0.87	280.0	70.0	70.0	0.0	60.0
N 18	55	607.600	0.04	0.93	280.0	70.0	70.0	0.0	60.0
N 19	1200	610.600	0.03	0.58	280.0	70.0	70.0	0.0	60.0
N 20	5	613.500	0.02	0.58	280.0	70.0	70.0	0.0	60.0
N 21	10	616.700	0.03	0.70	280.0	70.0	70.0	0.0	60.0
N 22	15	619.800	0.03	0.70	280.0	70.0	70.0	0.0	60.0
N 23	20	621.900	0.01	0.20	140.0	70.0	70.0	0.0	65.0
N 24	25	623.680	0.01	0.20	130.0	70.0	70.0	0.0	65.0
N 1	1255	627.300	0.04	1.05	280.0	70.0	70.0	0.0	60.0
N 2	1300	631.200	0.04	1.05	280.0	70.0	70.0	0.0	55.0
N 3	30	635.400	0.06	1.23	275.0	70.0	70.0	0.0	60.0
N 4	45	639.700	0.06	1.23	280.0	70.0	70.0	0.0	60.0

MARBLEHE

TRAVERSE SUMMARY (CONTINUED)

POINT NO.	CLOCK TIME	METER VOLUME	PITOT TUBE DELTAP	ORIFICE DELTAP	STACK TEMP.	METER TEMPERATURE INLET	TEMPERATURE OUTLET	PUMP VACUUM	IMPINGER TEMP.
	(MIN)	(GAL)	(IN. H ₂ O)	(IN. H ₂ O)	(DEG. F)	(DEG. F)	(DEG. F)	(IN. HG)	(DEG. F)
N 5	50	643.700	0.05	1.17	280.0	70.0	70.0	0.0	60.0
N 6	55	648.000	0.06	1.23	280.0	70.0	70.0	0.0	60.0
N 7	1400	652.500	0.06	1.40	280.0	70.0	70.0	0.0	60.0
N 8	5	656.800	0.06	1.35	280.0	70.0	70.0	0.0	60.0
N 9	15	661.000	0.05	1.20	280.0	70.0	70.0	0.0	60.0
N10	30	664.800	0.04	1.00	280.0	70.0	70.0	0.0	60.0
N11	35	668.700	0.04	1.05	275.0	70.0	70.0	0.0	55.0
N12	40	672.800	0.05	1.17	280.0	70.0	70.0	0.0	55.0
N13	45	676.900	0.05	1.17	280.0	70.0	70.0	0.0	55.0
N14	50	680.800	0.04	1.02	280.0	70.0	70.0	0.0	60.0
N15	55	684.700	0.04	1.05	285.0	70.0	70.0	0.0	60.0
N16	1500	688.400	0.04	0.98	280.0	70.0	70.0	0.0	60.0
N17	5	692.300	0.04	1.07	280.0	70.0	70.0	0.0	60.0
N18	10	696.200	0.04	1.07	285.0	70.0	70.0	0.0	60.0
N19	15	700.100	0.04	1.07	285.0	70.0	70.0	0.0	60.0
N20	20	704.000	0.04	1.07	285.0	70.0	70.0	0.0	60.0
N21	25	707.500	0.04	0.83	280.0	70.0	70.0	0.0	60.0
N22	30	710.900	0.04	0.83	285.0	70.0	70.0	0.0	60.0
N23	35	714.600	0.04	1.00	270.0	70.0	70.0	0.0	60.0
N24	40	717.600	0.03	0.58	280.0	70.0	70.0	0.0	60.0
AVERAGE OF 48 POINTS			0.04	0.89	269.3	70.0	70.0	0.0	59.4

MARBLEHE

PARTICULATE TEST SUMMARY-RUN NO. 4

STACK DATA

AVERAGE VELOCITY HEAD= 0.19
ACTUAL VELOCITY= 12.8 FEET PER SECOND (FPS)
PERCENT ISOKINETIC FLOW= 101.6 %
MOISTURE CONTENT= 7.5 %
MOLECULAR WEIGHT, WET BASIS= 28.90
VOLUMETRIC FLOW= 1274832.0 SCFH, DRY
1942475.0 ACFH
32374.6 ACFM

LABORATORY DATA

(Front Half Only)

FILTER CATCH = 32.4 MG.
FRONT HALF (ACETONE WASH) = 58.5 MG.
FRONT HALF (WATER WASH) = 27.2 MG.
BACK HALF (ACETONE WASH) = 31.7 MG.
BACK HALF (ORGANIC EXTRACT) = 4.5 MG.
BACK HALF (WATER RESIDUE) = 120.7 MG.
TOTAL PARTICULATE COLLECTED = 275.0 MG.

Front 1/2 118.1 mg; 1.98 lb/hr = 59.65 mg/hr

EMISSIONS

(Front Half Only)

-02
-06
IE GAS= 5.19E-02
1.09E-02
1.56E-06
1.98E-00
2.23E-02

ORGANIC : $4.5 \text{ mg} \times \frac{1}{14 \text{ hr}} = 59.65 \text{ mg/hr}$

$= 0.0754 \text{ lb/hr}$

INORGANIC $(31.7 + 120.7) \text{ mg} \times \frac{1}{14 \text{ hr}} = 59.65 \text{ mg/hr}$

$\approx 2.55 \text{ lb/hr}$

MARBLEHE

FIELD TEST DATA SUMMARY TEST NO. 5

PROBE LOCATION= STACK NO.5

COLLECTOR TYPE= EPA TRAIN

AMBIENT TEMPERATURE= 73.0 DEGREES FAHRENHEIT

BAROMETRIC PRESSURE= 29.21 INCHES MERCURY

PROBE LENGTH= 13.0 FEET

NOZZLE DIAMETER= 0.50 INCHES

PITOT TUBE CALIBRATION FACTOR= 0.43

STACK AREA= 42.24 SQ. FT.

GAS ANALYSIS

CO2= 7.0 %

CO = 0.0 %

O2 = 16.5 %

N2 = 76.5 %

MOLECULAR WEIGHT= 29.78 , DRY BASIS

EXCESS AIR= **** %

MARBLEHE

TRAVERSE SUMMARY (TEST NO. 5)

POINT NO.	CLOCK TIME	METER VOLUME	PITOT TUBE DELTAP	ORIFICE DELTAP	STACK TEMP.	METER TEMPERATURE INLET	TEMPERATURE OUTLET	PUMP VACUUM	IMPINGER TEMP.
	(MIN)	(GAL)	(IN. H ₂ O)	(IN. H ₂ O)	(DEG F)	(DEG F)	(DEG F)	(IN. HG)	(DEG F)
START	930	717.610							
N 1	35	721.900	0.06	1.25	280.0	70.0	70.0	0.0	55.0
N 2	40	726.300	0.06	1.28	285.0	70.0	70.0	0.0	55.0
N 3	45	730.600	0.06	1.32	280.0	70.0	70.0	0.0	55.0
N 4	50	734.700	0.05	1.22	280.0	70.0	70.0	0.0	60.0
N 5	55	739.000	0.06	1.32	280.0	70.0	70.0	0.0	60.0
N 6	100	743.600	0.07	1.52	280.0	70.0	70.0	0.0	60.0
N 7	5	748.300	0.07	1.55	280.0	70.0	70.0	0.0	60.0
N 8	10	752.900	0.07	1.55	285.0	70.0	70.0	0.0	60.0
N 9	15	757.300	0.06	1.32	280.0	70.0	70.0	0.0	60.0
N 10	20	761.700	0.06	1.45	280.0	70.0	70.0	0.0	60.0
N 11	25	766.200	0.06	1.47	280.0	70.0	70.0	0.0	60.0
N 12	30	770.700	0.06	1.47	280.0	70.0	70.0	0.0	60.0
N 13	35	774.470	0.04	0.88	280.0	70.0	70.0	0.0	60.0
N 14	40	777.900	0.04	0.98	280.0	70.0	70.0	0.0	60.0
N 15	45	781.600	0.04	0.90	280.0	70.0	70.0	0.0	60.0
N 16	50	785.600	0.05	1.22	280.0	70.0	70.0	0.0	60.0
N 17	55	789.600	0.04	1.02	280.0	70.0	70.0	0.0	65.0
N 18	1100	793.300	0.04	1.10	280.0	70.0	70.0	0.0	65.0
N 19	5	797.100	0.04	0.98	280.0	70.0	70.0	0.0	65.0
N 20	10	800.800	0.04	1.00	280.0	70.0	70.0	0.0	65.0
N 21	15	804.700	0.04	1.08	280.0	70.0	70.0	0.0	60.0
N 22	20	808.900	0.05	1.30	280.0	70.0	70.0	0.0	60.0
N 23	25	812.700	0.04	1.02	275.0	70.0	70.0	0.0	60.0
N 24	30	816.100	0.03	0.70	270.0	70.0	70.0	0.0	65.0
S 1	1205	820.500	0.04	0.98	280.0	70.0	70.0	0.0	70.0
S 2	10	824.300	0.04	0.98	280.0	70.0	70.0	0.0	60.0
S 3	15	827.100	0.04	1.00	285.0	70.0	70.0	0.0	60.0
S 4	20	832.200	0.07	0.0	285.0	70.0	70.0	0.0	60.0

MARBLEHE

TRAVERSE SUMMARY (CONTINUED)

POINT NO.	CLOCK TIME (MIN)	METER VOLUME (ACEL)	PITOT TUBE DELTAP (IN. H ₂ O)	ORIFICE DELTAP (IN. H ₂ O)	STACK TEMP. (DEG F)	METER TEMPERATURE INLET (DEG F)	METER TEMPERATURE OUTLET (DEG F)	PUMP VACUUM (IN. HG)	IMPINGER TEMP. (DEG F)
S 5	35	836.300	0.06	1.45	280.0	70.0	70.0	0.0	60.0
S 6	45	841.100	0.07	1.78	280.0	70.0	70.0	0.0	60.0
S 7	50	846.100	0.07	1.80	280.0	70.0	70.0	0.0	60.0
S 8	55	850.800	0.07	1.65	280.0	70.0	70.0	0.0	60.0
S 9	1300	855.600	0.07	1.67	275.0	70.0	70.0	0.0	60.0
S10	5	860.200	0.07	1.52	275.0	70.0	70.0	0.0	60.0
S11	10	864.700	0.07	1.52	275.0	70.0	70.0	0.0	60.0
S12	15	869.300	0.07	1.52	280.0	70.0	70.0	0.0	60.0
S13	20	874.200	0.07	1.52	280.0	70.0	70.0	0.0	60.0
S14	25	878.400	0.07	1.52	280.0	70.0	70.0	0.0	60.0
S15	30	881.900	0.04	0.82	280.0	70.0	70.0	0.0	60.0
S16	35	885.300	0.04	0.95	280.0	70.0	70.0	0.0	65.0
S17	40	889.000	0.04	0.98	280.0	70.0	70.0	0.0	65.0
S18	45	893.400	0.07	1.60	280.0	70.0	70.0	0.0	70.0
S19	50	898.300	0.07	1.75	280.0	70.0	70.0	0.0	70.0
S20	55	902.200	0.04	1.18	280.0	70.0	70.0	0.0	65.0
S21	1400	906.000	0.04	1.05	245.0	70.0	70.0	0.0	65.0
S22	5	908.800	0.03	1.10	230.0	70.0	70.0	0.0	65.0
S23	10	911.700	0.03	1.05	160.0	70.0	70.0	0.0	65.0
S24	15	914.470	0.02	0.50	110.0	70.0	70.0	0.0	65.0
AVERAGE OF 48 POINTS									
			0.05	1.22	272.0	70.0	70.0	0.0	61.6

MARBLEHE

PARTICULATE TEST SUMMARY-RUN NO. 5

SIACK DATA

AVERAGE VELOCITY HEAD= 0.23
ACTUAL VELOCITY= 15.0 FEET PER SECOND (FPS)
PERCENT ISOKINETIC FLOW= 100.0 %
MOISTURE CONTENT= 7.4 %
MOLECULAR WEIGHT, WET BASIS= 28.90
VOLUMETRIC FLOW= 1492680.0 SCFH, DRY
2281456.0 ACFM
38024.3 ACFM

LABORATORY DATA

(Front Half Only)

FILTER CATCH	=	69.4 MG.
FRONT HALF (ACETONE WASH)	=	65.5 MG.
FRONT HALF (WATER WASH)	=	21.3 MG.
BACK HALF (ACETONE WASH)	=	60.3 MG.
BACK HALF (ORGANIC EXTRACT)	=	6.0 MG.
BACK HALF (WATER RESIDUE)	=	97.9 MG.
TOTAL PARTICULATE COLLECTED	=	320.4 MG.

FRONT 1/2 156.2 mg: 2.67 $\frac{1}{hr}$ = 58.5 $\frac{mg}{hr}$ ¹⁵SIONS

(Front Half Only)
1.25 E-02
1.79E-06
2.67E-00
2.56E-02

ORGANIC 6.04 * $\frac{1}{58.5 \frac{mg}{hr}}$ IS= 5.25E-02

= 0.103 $\frac{1}{hr}$

INORGANIC : $(60.3 + 97.9) \frac{mg}{hr} \times \frac{1}{58.5}$
2.70

MARBLEHE

FIELD TEST DATA SUMMARY TEST NO. 6

PROBE LOCATION= STACK NO.6

COLLECTOR TYPE= EPA TRAIN

AMBIENT TEMPERATURE= 73.0 DEGREES FAHRENHEIT

BAROMETRIC PRESSURE= 29.21 INCHES MERCURY

PROBE LENGTH= 13.0 FEET

NOZZLE DIAMETER= 0.50 INCHES

PITOT TUBE CALIBRATION FACTOR= 0.83

STACK AREA= 42.24 SQ. FT.

GAS ANALYSIS

CO2= 7.0 %

CO = 0.0 %

O2 = 16.5 %

N2 = 76.5 %

MOLECULAR WEIGHT= 29.78 , DRY BASIS

EXCESS AIR= **** %

MARBLEHE

TRAVERSE SUMMARY (TEST NO. 6)

POINT NO.	CLOCK TIME	METER VOLUME	PITOT TUBE DELTAP	ORIFICE DELTAP	STACK TEMP.	METER INLET	TEMPERATURE OUTLET	PUMP VACUUM	IMPINGER TEMP.
	(MIN)	(ACE)	(IN. H ₂ O)	(IN. H ₂ O)	(DEG F)	(DEG F)	(DEG F)	(IN. HG)	(DEG F)
START	925	790.120							
N24	30	794.200	0.05	1.05	270.0	70.0	70.0	0.0	70.0
N23	35	798.400	0.05	1.00	270.0	70.0	70.0	0.0	60.0
N22	40	802.600	0.06	1.20	270.0	70.0	70.0	0.0	65.0
N21	45	807.100	0.06	1.30	280.0	70.0	70.0	0.0	70.0
N20	50	811.600	0.06	1.30	280.0	70.0	70.0	0.0	70.0
N19	55	816.100	0.06	1.30	280.0	70.0	70.0	0.0	70.0
N18	1000	820.200	0.05	1.15	275.0	70.0	70.0	0.0	70.0
N17	5	824.300	0.05	1.15	270.0	70.0	70.0	0.0	65.0
N16	10	828.500	0.05	1.20	275.0	70.0	70.0	0.0	65.0
N15	15	832.800	0.05	1.20	280.0	70.0	70.0	0.0	60.0
N14	20	837.000	0.05	1.20	275.0	70.0	70.0	0.0	60.0
N13	25	840.800	0.05	1.00	275.0	70.0	70.0	0.0	65.0
N12	30	845.000	0.05	1.20	270.0	70.0	70.0	0.0	65.0
N11	35	849.300	0.05	1.20	270.0	70.0	70.0	0.0	65.0
N10	40	853.400	0.05	1.20	270.0	70.0	70.0	0.0	65.0
N 9	45	857.700	0.05	1.20	270.0	70.0	70.0	0.0	70.0
N 8	50	861.800	0.05	1.20	260.0	70.0	70.0	0.0	70.0
N 7	55	866.800	0.05	1.20	260.0	70.0	70.0	0.0	65.0
N 6	1100	869.700	0.04	1.00	265.0	70.0	70.0	0.0	65.0
N 5	5	872.800	0.03	0.80	260.0	70.0	70.0	0.0	60.0
N 4	10	876.600	0.03	0.80	260.0	70.0	70.0	0.0	60.0
N 3	15	879.800	0.03	0.60	260.0	70.0	70.0	0.0	60.0
N 2	20	882.500	0.02	0.60	260.0	70.0	70.0	0.0	65.0
N 1	25	885.100	0.02	0.50	255.0	70.0	70.0	0.0	65.0
S24	1205	889.300	0.05	1.20	280.0	70.0	70.0	0.0	65.0
S23	10	893.400	0.05	1.20	275.0	70.0	70.0	0.0	60.0
S22	15	897.500	0.05	1.15	280.0	70.0	70.0	0.0	65.0
S21	20	901.600	0.05	1.20	280.0	70.0	70.0	0.0	60.0

MARBLEHE

TRAVERSE SUMMARY (CONTINUED)

POINT NO.	CLOCK TIME	METER VOLUME	PILOT TUBE DELTAP	ORIFICE (IN. H ₂ O)	STACK TEMP. (DEG F)	METER INLET TEMP. (DEG F)	METER OUTLET TEMP. (DEG F)	PUMP VACUUM (IN. HG)	IMPINGER TEMP. (DEG F)
S20	25	905.800	0.05	1.20	280.0	70.0	70.0	0.0	60.0
S19	30	910.200	0.06	1.35	280.0	70.0	70.0	0.0	65.0
S18	35	914.700	0.06	1.35	280.0	70.0	70.0	0.0	65.0
S17	40	919.300	0.06	1.40	280.0	70.0	70.0	0.0	70.0
S16	45	923.400	0.05	1.20	280.0	70.0	70.0	0.0	70.0
S15	50	927.500	0.05	1.20	280.0	70.0	70.0	0.0	65.0
S14	55	931.700	0.05	1.20	280.0	70.0	70.0	0.0	65.0
S13	1300	935.900	0.05	1.20	275.0	70.0	70.0	0.0	60.0
S12	5	939.200	0.03	0.50	280.0	70.0	70.0	0.0	65.0
S11	10	942.100	0.03	0.50	275.0	70.0	70.0	0.0	65.0
S10	15	945.000	0.03	0.50	275.0	70.0	70.0	0.0	65.0
S9	20	948.100	0.03	0.60	275.0	70.0	70.0	0.0	65.0
S8	25	951.200	0.03	0.70	275.0	70.0	70.0	0.0	65.0
S7	30	954.800	0.04	0.90	280.0	70.0	70.0	0.0	65.0
S6	35	958.500	0.04	0.90	275.0	70.0	70.0	0.0	65.0
S5	40	961.700	0.03	0.60	280.0	70.0	70.0	0.0	65.0
S4	45	964.900	0.03	0.70	270.0	70.0	70.0	0.0	65.0
S3	50	968.600	0.04	0.90	270.0	70.0	70.0	0.0	65.0
S2	55	972.700	0.04	0.90	270.0	70.0	70.0	0.0	70.0
S1	1400	976.430	0.04	0.90	270.0	70.0	70.0	0.0	70.0
AVERAGE OF 48 POINTS		0.04	1.02	273.0	70.0	70.0	0.0	65.1	

MARBLEHE

PARTICULATE TEST SUMMARY-RUN NO. 6

SIACK DATA

AVERAGE VELOCITY HEAD= 0.21
ACTUAL VELOCITY= 13.8 FEET PER SECOND (FPS)
PERCENT ISOINETIC FLOW= 101.6 %
MOISTURE CONTENT= 6.5 %
MOLECULAR WEIGHT, WET BASIS= 29.02
VOLUMETRIC FLOW= 1389359.0 SCFH, DRY
2104649.0 ACFH
35077.5 ACFM

LABORATORY DATA

(Front Half Only)

FILTER CATCH	=	47.0 MG.
FRONT HALF (ACETONE WASH)	=	63.8 MG.
FRONT HALF (WATER WASH)	=	26.2 MG.
BACK HALF (ACETONE WASH)	=	22.2 MG.
BACK HALF (ORGANIC EXTRACT)	=	5.2 MG.
BACK HALF (WATER RESIDUE)	=	212.6 MG.
TOTAL PARTICULATE COLLECTED	=	377.0 MG.

FRONT Σ : 137.0 mg : 2.316/hr = 59.57 $\frac{\text{mg}}{\text{hr}}$ LONS

(Front Half Only)
1.16E-02
1.66E-06
2.30E-00
2.36E-02

ORGANIC : 5.2 mg $\times$ 59.57 $\frac{\text{mg}}{\text{hr}}$
= 0.873 $\frac{\text{mg}}{\text{hr}}$
= 6.50E-02

NO ORGANIC : (2.2 + 212.6) $\times$ 59.57
= 3.94

SAMPLE CALCULATIONS

TEST NO. 1

1. VOLUME OF DRY GAS SAMPLED AT STANDARD CONDITIONS, DSCF

$$V_{mSTD} = \frac{17.71 \times V_m \left(P_b + \frac{\Delta H}{13.6} \right)}{(T_m + 460)} = \frac{(17.71)(186.31)(29.10 + \frac{.99}{13.6})}{530} = 181.62$$

2. VOLUME OF WATER VAPOR AT STANDARD CONDITIONS, SCF

$$V_{WSTD} = (0.0474) V_{LC} = (0.0474)(265) = 12.56$$

3. MOISTURE CONTENT IN STACK GAS

$$B_{W0} = \frac{V_{WSTD}}{V_{mSTD} + V_{WSTD}} = \frac{12.56}{181.62 + 12.56} = 0.065 \quad \text{6.5\% moisture}$$

4. MOLE FRACTION OF DRY GAS

$$M_D = \frac{100 - 100(B_{W0})}{100} = \frac{100 - 100(.065)}{100} = 0.935$$

5. MOLECULAR WEIGHT OF DRY STACK GAS, lb/lb-mole

$$\begin{aligned} M_{WD} &= (0.44)(\%CO_2) + (0.32)(\%O_2) + (0.28)(\%N_2 + \%CO) \\ &= .44(6.8) + .32(19.5) + .28(73.7) = 29.87 \text{ lb/lb-mole} \end{aligned}$$

6. MOLECULAR WEIGHT OF WET STACK GAS, lb/lb-mole

$$M_w = M_{wD} \times M_D + 18(1 - M_D) = 29.87 \times .935 + 18(1 - .935) = 29.10 \frac{\text{lb}}{\text{lb-mole}}$$

7. STACK GAS VELOCITY AT STACK CONDITIONS, fpm

$$V_s = 5128.8 \times C_p \times (\sqrt{\Delta P})_{\text{avg.}} \sqrt{\frac{T_{s\text{avg.}}}{P_s M_w}}$$

$$5128.8 \times .83 \times .22 \sqrt{\frac{751}{(29.10)(29.10)}} = 881.9 \text{ fpm}$$

8. STACK GAS VOLUMETRIC FLOW RATE AT STACK CONDITIONS, DSCFM

$$Q_s = (1 - B_{w0})(V_s)(A) \left(\frac{T_{STD}}{T_{s\text{avg.}}} \right) \left(\frac{P_s}{P_{STD}} \right) =$$

$$(1 - .065)(881.9)(42.24) \left(\frac{530}{751} \right) \left(\frac{29.10}{29.92} \right) = 23,907 \text{ DSCFM}$$

9. STACK VOLUMETRIC FLOW RATE AT STACK CONDITIONS, ACFM

$$Q_D = \frac{Q_s (T_s + 460)(29.92)}{530(P_s)(M_D)} = \frac{(23,907)(751)(29.92)}{530(29.10)(.935)} = 37,252 \text{ ACFM}$$

$\uparrow$
(P_{STD})

10. PERCENT ISO-KINETIC

$$\Sigma I = \frac{1,032 \times (T_s + 460) V_{mSTD}}{V_s \times T_s \times P_s \times M_D \times D_N^2} = \frac{(1032)(751)(181.62)}{(881.9)(240)(29.10)(.935)(.5)^2} = 97.8\%$$

1. PARTICULATE - PROBE + FILTER, GR./DSCF

$$C_{an} = 0.0154 \times \frac{M_f}{V_{mSTD}} = 0.0154 \times \frac{262.4}{181.62} = 0.0222 \text{ GR./DSCF}$$

2. PARTICULATE - TOTAL, GR./DSCF

$$C_{ao} = 0.0154 \times \frac{M_t}{V_{mSTD}} = 0.0154 \times \frac{424.5}{181.62} = 0.0360 \text{ GR./DSCF}$$

3. PARTICULATES - PROBE + FILTER AT STACK CONDITIONS, GR./ACF

$$C_{at} = \frac{17.71 \times C_{an} \times P_s \times M_D}{(T_s + 460)} = \frac{17.71 \times 0.0223 \times 29.10 \times .935}{751} = 0.0143 \text{ GR./ACF}$$

4. PARTICULATES - TOTAL AT STACK CONDITIONS, GR./ACF

$$C_{au} = \frac{17.71 (C_{ao}) \times P_s \times M_D}{(T_s + 460)} = \frac{17.71 \times 0.0361 \times 29.1 \times .935}{751} = 0.0231 \text{ GR./ACF}$$

5. PARTICULATES - PROBE + FILTER, LB/HR.

$$C_{aw} = 0.00857 \times C_{an} \times Q_s = 0.00857 \times 0.0222 \times 23,907 = 4.55 \text{ LB/HR}$$

6. PARTICULATES - PROBE + FILTER, LBS/HR.

$$C_{ax} = 0.00857 \times C_{ao} \times Q_s = 0.00857 \times 0.036 \times 23,907 = 7.38 \text{ LBS/HR}$$

17. PARTICULATE - probe, cyclone, and filter, lb/ton feed

$$P_{tf} = \frac{C_{aw}}{T_c} = \frac{4.55}{37.76} = 0.1205 \text{ lb/ton}$$

18. PARTICULATE - total, lb/ton feed

$$P_{tt} = \frac{C_{ax}}{T_c} = \frac{7.38}{37.76} = 0.1949 \text{ lb/ton}$$

APPENDIX B
SULFUR DIOXIDE TEST RESULTS
AND SAMPLE CALCULATION

WALDEN SOURCE TEST REPORT

COMPANY= MARBLEHEAD LIME COMPANY

PLANT= LIME KILN NUMBER 5

LOCATION= GARY, INDIANA

PROCESS= LIME KILN

CONTROL EQUIPMENT= BAGHOUSE

TEST SCHEDULE

RUN NO.	DATE	POLLUTANTS SAMPLED				
1	11JUN 74	PAHT	SO2	NOX	CO	OPACITY
2	11JUN 74	PAHT	SO2			OPACITY
3	12JUN 74	PAHT	SO2	NOX	CO	OPACITY
4	12JUN 74	PAHT	SO2			OPACITY
5	13JUN 74	PAHT	SO2	NOX	CO	OPACITY
6	13JUN 74	PAHT	SO2			OPACITY

MARBLEHE

S02 TEST SUMMARY-RUN NO. 1
BASED ON METHOD 5 TRAVERSE

STACK DATA

ACTUAL VELOCITY= 14.6 FEET PER SECOND(FPS)
MOISTURE CONTENT= 6.5 %
VOLUMETRIC FLOW= 1427802.0 SCFH, DRY
2222941.0 ACFH
37049.0 ACFM

LABORATORY DATA

REPLICATE NO.= 1
TITRANT VOLUME= 7.350 ML
BLANK VOLUME= 0.0 ML
TITRANT NORMALITY=0.01030N
SOLUTION VOLUME= 100.0 ML
ALIQOT VOLUME= 20.0 ML
S02 CONCENTRATION= 1.32E-05 POUNDS/SCF, DRY

REPLICATE NO.= 2
TITRANT VOLUME= 7.350 ML
BLANK VOLUME= 0.0 ML
TITRANT NORMALITY=0.01030N
SOLUTION VOLUME= 100.0 ML
ALIQOT VOLUME= 20.0 ML
S02 CONCENTRATION= 1.32E-05 POUNDS/SCF, DRY

S02 RESULTS(AVERAGE OF 2 REPLICATES)

POUNDS/SCF, DRY= 1.32E-05
POUNDS/HOUR= 1.89E 01

PPM(VOLUME)= 8.09E 01 (@25 DEG C.)

MARBLEHE

S02

TEST SUMMARY-RUN NO. 2
BASED ON METHOD 5 TRAVERSE

STACK DATA

ACTUAL VELOCITY= 13.0 FEET PER SECOND (FPS)
MOISTURE CONTENT= 4.8 %
VOLUMETRIC FLOW= 1344402.0 SCFH, DRY
1981892.0 ACFH
33031.5 ACFM

LABORATORY DATA

REPLICATE NO.= 1
TITRANT VOLUME= 4.150 ML
BLANK VOLUME= 0.0 ML
TITRANT NORMALITY=0.01030N
SOLUTION VOLUME= 100.0 ML
ALIQOT VOLUME= 20.0 ML
SO2 CONCENTRATION= 1.27E-05 POUNDS/SCF, DRY

REPLICATE NO.= 2
TITRANT VOLUME= 4.100 ML
BLANK VOLUME= 0.0 ML
TITRANT NORMALITY=0.01030N
SOLUTION VOLUME= 100.0 ML
ALIQOT VOLUME= 20.0 ML
SO2 CONCENTRATION= 1.26E-05 POUNDS/SCF, DRY

SO2 RESULTS (AVERAGE OF 2 REPLICATES)

POUNDS/SCF, DRY= 1.27E-05
POUNDS/HOUR= 1.70E 01

PPM (VOLUME)= 7.74E 01 (#25 DEG C.)

MARBLEHE

S02

TEST SUMMARY-RUN NO. 3
BASED ON METHOD 5 TRAVERSE

STACK DATA

ACTUAL VELOCITY= 14.0 FEET PER SECOND (FPS)
MOISTURE CONTENT= 6.3 %
VOLUMETRIC FLOW= 1389731.0 SCFH, DRY
2131933.0 ACFH
35532.2 ACFM

LABORATORY DATA

REPLICATE NO.= 1
TITRANT VOLUME= 7.560 ML
BLANK VOLUME= 0.0 ML
TITRANT NORMALITY=0.01030N
SOLUTION VOLUME= 100.0 ML
ALIQOUT VOLUME= 20.0 ML
SO2 CONCENTRATION= 1.74E-05 POUNDS/SCF, DRY

REPLICATE NO.= 2
TITRANT VOLUME= 7.590 ML
BLANK VOLUME= 0.0 ML
TITRANT NORMALITY=0.01030N
SOLUTION VOLUME= 100.0 ML
ALIQOUT VOLUME= 20.0 ML
SO2 CONCENTRATION= 1.74E-05 POUNDS/SCF, DRY

SO2 RESULTS (AVERAGE OF 2 REPLICATES)

POUNDS/SCF, DRY= 1.74E-05
POUNDS/HOUR= 2.42E 01

PPM (VOLUME)= 1.06E 02 (@25 DEG C.)

MARBLEHE

S02

TEST SUMMARY-RUN NO. 4
BASED ON METHOD 5 TRAVERSE

STACK DATA

ACTUAL VELOCITY= 12.8 FEET PER SECOND (FPS)
MOISTURE CONTENT= 7.5 %
VOLUMETRIC FLOW= 1274832.0 SCFH, DRY
1942475.0 ACFH
32374.6 ACFM

LABORATORY DATA

REPLICATE NO.= 1
TITRANT VOLUME= 6.270 ML
BLANK VOLUME= 0.0 ML
TITRANT NORMALITY=0.01030N
SOLUTION VOLUME= 100.0 ML
ALiquot VOLUME= 20.0 ML
SO2 CONCENTRATION= 1.46E-05 POUNDS/SCF, DRY

REPLICATE NO.= 2
TITRANT VOLUME= 6.450 ML
BLANK VOLUME= 0.0 ML
TITRANT NORMALITY=0.01030N
SOLUTION VOLUME= 100.0 ML
ALiquot VOLUME= 20.0 ML
SO2 CONCENTRATION= 1.50E-05 POUNDS/SCF, DRY

SO2 RESULTS (AVERAGE OF 2 REPLICATES)

POUNDS/SCF, DRY= 1.48E-05
POUNDS/HOUR= 1.89E 01

PPM (VOLUME)= 9.07E 01 (@25 DEG C.)

MARBLEHE

S02 TEST SUMMARY-RUN NO. 5
BASED ON METHOD 5 TRAVERSE

STACK DATA

ACTUAL VELOCITY= 15.0 FEET PER SECOND (FPS)
MOISTURE CONTENT= 7.4 %
VOLUMETRIC FLOW= 1492680.0 SCFH, DRY
2281456.0 ACFH
38024.3 ACFM

LABORATORY DATA

REPLICATE NO.= 1
TITRANT VOLUME= 6.000 ML
BLANK VOLUME= 0.0 ML
TITRANT NORMALITY=0.01030N
SOLUTION VOLUME= 121.0 ML
ALIQOT VOLUME= 20.0 ML
S02 CONCENTRATION= 1.63E-05 POUNDS/SCF, DRY

REPLICATE NO.= 2
TITRANT VOLUME= 6.050 ML
BLANK VOLUME= 0.0 ML
TITRANT NORMALITY=0.01030N
SOLUTION VOLUME= 121.0 ML
ALIQOT VOLUME= 20.0 ML
S02 CONCENTRATION= 1.64E-05 POUNDS/SCF, DRY

S02 RESULTS (AVERAGE OF 2 REPLICATES)

POUNDS/SCF, DRY= 1.64E-05
POUNDS/HOUR= 2.44E 01

PPM (VOLUME)= 1.00E 02 (@25 DEG C.)

MARBLEHE

SO2

TEST SUMMARY-RUN NO. 6
BASED ON METHOD 5 TRAVERSE

STACK DATA

ACTUAL VELOCITY= 13.8 FEET PER SECOND (FPS)
MOISTURE CONTENT= 6.5 %
VOLUMETRIC FLOW= 1389359.0 SCFH, DRY
2104649.0 ACFH
35077.5 ACFM

LABORATORY DATA

REPLICATE NO.= 1
TITRANT VOLUME= 3.750 ML
BLANK VOLUME= 0.0 ML
TITRANT NORMALITY=0.01030N
SOLUTION VOLUME= 117.0 ML
ALiquot VOLUME= 20.0 ML
SO2 CONCENTRATION= 1.55E-05 POUNDS/SCF, DRY

REPLICATE NO.= 2
TITRANT VOLUME= 3.750 ML
BLANK VOLUME= 0.0 ML
TITRANT NORMALITY=0.01030N
SOLUTION VOLUME= 117.0 ML
ALiquot VOLUME= 20.0 ML
SO2 CONCENTRATION= 1.55E-05 POUNDS/SCF, DRY

SO2 RESULTS (AVERAGE OF 2 REPLICATES)

POUNDS/SCF, DRY= 1.55E-05
POUNDS/HOUR= 2.15E 01

PPM (VOLUME)= 9.48E 01 (@25 DEG C.)

SAMPLE CALCULATIONS

TEST NO. 1

1. VOLUME OF GAS SAMPLE THROUGH DRY GAS METER, DSCF

$$V_{mSTD} = \frac{(17.71)(V_m)(P_{bar})}{T_m} = \frac{(17.71)(2.08)(29.10)}{532} = 2.01 \text{ DSCF}$$

2. SULFUR DIOXIDE CONCENTRATION, LBS./DSCF

$$C_{SO_2} = \frac{(7.05 \times 10^{-5})(V_f - V_i)(N)\left(\frac{V_{soln}}{V_a}\right)}{V_{mSTD}} =$$

$$= \frac{(7.05 \times 10^{-5})(7.35)(.0103)\left(\frac{100}{20}\right)}{2.01} = 1.32 \times 10^{-5} \frac{\text{LBS}}{\text{DSCF}}$$

3. SULFUR DIOXIDE CONCENTRATION, PPM

$$C_{PPM} = C_{SO_2} \times \frac{359}{m_{w_{SO_2}}} \times \frac{T_{25}}{T_0} \times 10^6 = 1.32 \times 10^{-5} \times \frac{359}{64} \times \frac{298}{273} \times 10^6 =$$

$$= 80.8 \text{ PPM}$$

4. SULFUR DIOXIDE - TOTAL, LBS/HR.

$$C = (C_{SO_2})(Q_s)(60) = (1.32 \times 10^{-5})(23,797)(60) = 18.8 \text{ LBS/HR.}$$

APPENDIX C

NITROGEN OXIDES TEST RESULTS
AND SAMPLE CALCULATION

WALDEN SOURCE TEST REPORT

COMPANY= MARBLEHEAD LIME COMPANY

PLANT= LIME KILN NUMBER 5

LOCATION= GARY, INDIANA

PROCESS= LIME KILN

CONTROL EQUIPMENT= BAGHOUSE

TEST SCHEDULE

RUN NO.		DATE	POLLUTANTS SAMPLED				
1	11JUN 74	PART	S02	NOX	CO	OPACITY	
2	11JUN 74	PART	S02			OPACITY	
3	12JUN 74	PART	S02	NOX	CO	OPACITY	
4	12JUN 74	PART	S02			OPACITY	
5	13JUN 74	PART	S02	NOX	CO	OPACITY	
6	13JUN 74	PART	S02			OPACITY	

MARBLEHE

NOX TEST SUMMARY-RUN NO. 1
BASED ON METHOD 5 TRAVERSE

STACK DATA

ACTUAL VELOCITY= 14.6 FEET PER SECOND(FPS)
MOISTURE CONTENT= 6.5 %
VOLUMETRIC FLOW= 1427802.0 SCFH, DRY
2222941.0 ACFH
37049.0 ACFM

LABORATORY DATA

REPLICATE NO.= 1
FLASK VOLUME= 2038.0 ML
ABSORBANT VOLUME= 26.0 ML
INITIAL PRESSURE= 1.89 IN.HG
FINAL VOLUME= 29.41 IN.HG
INITIAL TEMPERATURE= 72.0 DEG. FAHRENHEIT
FINAL TEMPERATURE= 76.0 DEG. FAHRENHEIT
NOX CONCENTRATION= 4.94E-06 POUNDS/SCF, DRY (AS NO2)

REPLICATE NO.= 2
FLASK VOLUME= 2030.0 ML
ABSORBANT VOLUME= 24.5 ML
INITIAL PRESSURE= 1.89 IN.HG
FINAL VOLUME= 28.51 IN.HG
INITIAL TEMPERATURE= 70.0 DEG. FAHRENHEIT
FINAL TEMPERATURE= 74.0 DEG. FAHRENHEIT
NOX CONCENTRATION= 4.62E-06 POUNDS/SCF, DRY (AS NO2)

REPLICATE NO.= 3
FLASK VOLUME= 1961.0 ML
ABSORBANT VOLUME= 24.0 ML
INITIAL PRESSURE= 1.79 IN.HG
FINAL VOLUME= 28.61 IN.HG
INITIAL TEMPERATURE= 73.0 DEG. FAHRENHEIT
FINAL TEMPERATURE= 73.0 DEG. FAHRENHEIT
NOX CONCENTRATION= 4.99E-06 POUNDS/SCF, DRY (AS NO2)

REPLICATE NO.= 4
FLASK VOLUME= 1992.0 ML
ABSORBANT VOLUME= 25.5 ML
INITIAL PRESSURE= 1.89 IN.HG
FINAL VOLUME= 29.41 IN.HG
INITIAL TEMPERATURE= 72.0 DEG. FAHRENHEIT
FINAL TEMPERATURE= 74.0 DEG. FAHRENHEIT
NOX CONCENTRATION= 5.07E-06 POUNDS/SCF, DRY (AS NO2)

NOX RESULTS(AVERAGE OF 4 REPLICATES)

POUNDS/SCF, DRY= 4.90E-06
POUNDS/HOUR= 7.00E 00

PPM(VOLUME)= 4.18E 01 (@25 DEG C.)

MARBLEHE

NOX TEST SUMMARY-RUN NO. 3
BASED ON METHOD 5 TRAVERSE

STACK DATA

ACTUAL VELOCITY= 14.0 FEET PER SECOND (FPS)
MOISTURE CONTENT= 6.3 %
VOLUMETRIC FLOW= 1389731.0 SCFH, DRY
2131933.0 ACFM
35532.2 ACFM

LABORATORY DATA

REPLICATE NO.= 1
FLASK VOLUME= 1964.0 ML
ABSORBANT VOLUME= 25.0 ML
INITIAL PRESSURE= 2.04 IN.HG
FINAL VOLUME= 29.68 IN.HG
INITIAL TEMPERATURE= 72.0 DEG. FAHRENHEIT
FINAL TEMPERATURE= 80.0 DEG. FAHRENHEIT
NOX CONCENTRATION= 5.05E-06 POUNDS/SCF, DRY (AS NO2)

REPLICATE NO.= 2
FLASK VOLUME= 2046.0 ML
ABSORBANT VOLUME= 25.0 ML
INITIAL PRESSURE= 1.81 IN.HG
FINAL VOLUME= 29.06 IN.HG
INITIAL TEMPERATURE= 75.0 DEG. FAHRENHEIT
FINAL TEMPERATURE= 81.0 DEG. FAHRENHEIT
NOX CONCENTRATION= 4.92E-06 POUNDS/SCF, DRY (AS NO2)

REPLICATE NO.= 3
FLASK VOLUME= 2009.0 ML
ABSORBANT VOLUME= 25.0 ML
INITIAL PRESSURE= 1.80 IN.HG
FINAL VOLUME= 29.14 IN.HG
INITIAL TEMPERATURE= 76.0 DEG. FAHRENHEIT
FINAL TEMPERATURE= 81.0 DEG. FAHRENHEIT
NOX CONCENTRATION= 4.12E-06 POUNDS/SCF, DRY (AS NO2)

REPLICATE NO.= 4
FLASK VOLUME= 2020.0 ML
ABSORBANT VOLUME= 24.0 ML
INITIAL PRESSURE= 1.78 IN.HG
FINAL VOLUME= 28.88 IN.HG
INITIAL TEMPERATURE= 71.0 DEG. FAHRENHEIT
FINAL TEMPERATURE= 82.0 DEG. FAHRENHEIT
NOX CONCENTRATION= 3.77E-06 POUNDS/SCF, DRY (AS NO2)

NOX RESULTS (AVERAGE OF 4 REPLICATES)

POUNDS/SCF, DRY= 4.47E-06
POUNDS/HOUR= 6.21E 00

PPM (VOLUME)= 3.81E 01 (@25 DEG C.)

MARBLEHE

NOX TEST SUMMARY-RUN NO. 5
BASED ON METHOD 5 TRAVERSE

STACK DATA

ACTUAL VELOCITY= 15.0 FEET PER SECOND (FPS)
MOISTURE CONTENT= 7.4 %
VOLUMETRIC FLOW= 1492680.0 SCFH, DRY
2281456.0 ACFH
38024.3 ACFM

LABORATORY DATA

REPLICATE NO.= 1
FLASK VOLUME= 2030.0 ML
ABSORBANT VOLUME= 26.0 ML
INITIAL PRESSURE= 1.62 IN.HG
FINAL VOLUME= 29.67 IN.HG
INITIAL TEMPERATURE= 77.0 DEG. FAHRENHEIT
FINAL TEMPERATURE= 85.0 DEG. FAHRENHEIT
NOX CONCENTRATION= $9.48\text{E}-06$ POUNDS/SCF, DRY (AS NO2)

REPLICATE NO.= 2
FLASK VOLUME= 1992.0 ML
ABSORBANT VOLUME= 26.0 ML
INITIAL PRESSURE= 1.59 IN.HG
FINAL VOLUME= 29.57 IN.HG
INITIAL TEMPERATURE= 78.0 DEG. FAHRENHEIT
FINAL TEMPERATURE= 85.0 DEG. FAHRENHEIT
NOX CONCENTRATION= $7.70\text{E}-06$ POUNDS/SCF, DRY (AS NO2)

REPLICATE NO.= 3
FLASK VOLUME= 2040.0 ML
ABSORBANT VOLUME= 25.0 ML
INITIAL PRESSURE= 1.62 IN.HG
FINAL VOLUME= 29.47 IN.HG
INITIAL TEMPERATURE= 82.0 DEG. FAHRENHEIT
FINAL TEMPERATURE= 86.0 DEG. FAHRENHEIT
NOX CONCENTRATION= $9.15\text{E}-06$ POUNDS/SCF, DRY (AS NO2)

REPLICATE NO.= 4
FLASK VOLUME= 1994.0 ML
ABSORBANT VOLUME= 26.0 ML
INITIAL PRESSURE= 1.68 IN.HG
FINAL VOLUME= 29.37 IN.HG
INITIAL TEMPERATURE= 80.0 DEG. FAHRENHEIT
FINAL TEMPERATURE= 83.0 DEG. FAHRENHEIT
NOX CONCENTRATION= $7.87\text{E}-06$ POUNDS/SCF, DRY (AS NO2)

NOX RESULTS (AVERAGE OF 4 REPLICATES)

POUNDS/SCF, DRY= $8.55\text{E}-06$
POUNDS/HOUR= 1.28E 01

PPM (VOLUME)= 7.29E 01 (#25 DEG C.)

SAMPLE CALCULATION

No. 1 TEST

1. VOLUME OF GAS SAMPLE, MLS, DRY

$$V_{sc} = \frac{T_{STD} (V_f - V_a)}{P_{STD}} \left(\frac{P_f}{T_f} - \frac{P_i}{T_i} \right) = 17.71 (2038 - 26) \left(\frac{29.41}{536} - \frac{1.89}{532} \right) =$$

$$= 1828.7 \text{ MLS.}$$

2. NITROGEN OXIDES CONCENTRATION, LBS/SCF, DRY 25°C

$$C_{NOx} = 6.2 \times 10^{-5} \left(\frac{M}{V_{sc}} \right) = 6.2 \times 10^{-5} \left(\frac{145.6}{1828.7} \right) = 49.4 \times 10^{-7} \text{ LBS/SCF}$$

3. NITROGEN OXIDES CONCENTRATION, PPM 0°C

$$C_{PPM} = C_{NOx} \times \frac{359}{46} \times \frac{T_{25}}{T_0} \times 10^6 = \left(49.4 \times 10^{-7} \right) \left(\frac{359}{46} \right) \left(\frac{298}{273} \right) \times 10^6 =$$

$$= 42.1 \text{ PPM}$$

4. NITROGEN OXIDES - TOTAL, LBS/HR.

$$C = (C_{NOx})(Q_s)(60) = (49.4 \times 10^{-7})(23,797)(60) = 7.05 \text{ LBS/HR}$$

APPENDIX D
CARBON MONOXIDE TEST RESULTS

WALDEN SOURCE TEST REPORT

COMPANY= MARBLEHEAD LIME COMPANY

PLANT= LIME KILN NUMHER 5

LOCATION= GARY, INDIANA

PROCESS= LIME KILN

CONTROL EQUIPMENT= BAGHOUSE

TEST SCHEDULE

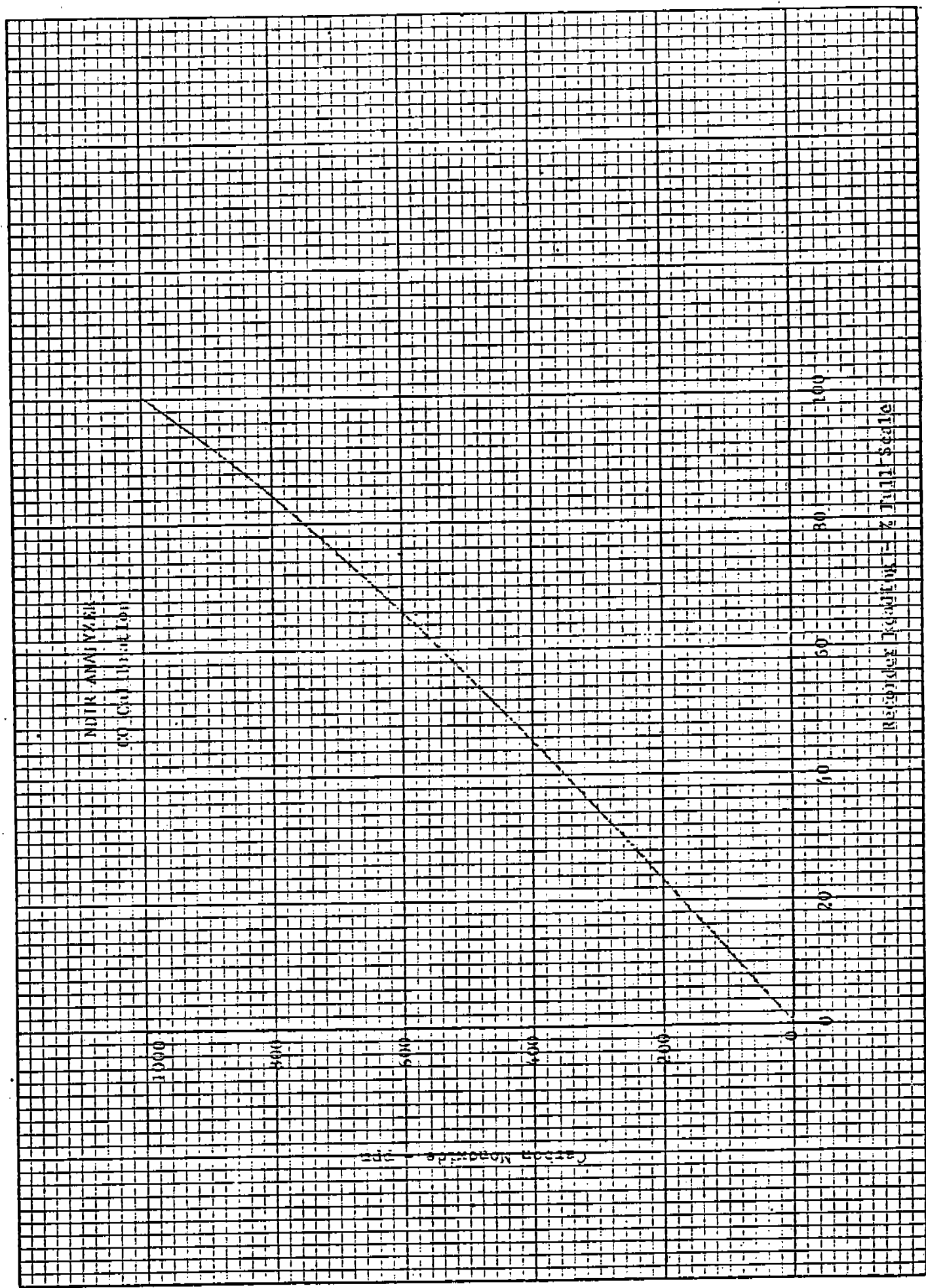
RUN NO.		DATE	POLLUTANTS SAMPLED			
1	11JUN 74	PART	S02	NOX	CO	OPACITY
2	11JUN 74	PART	S02			OPACITY
3	12JUN 74	PART	S02	NOX	CO	OPACITY
4	12JUN 74	PART	S02			OPACITY
5	13JUN 74	PART	S02	NOX	CO	OPACITY
6	13JUN 74	PART	S02			OPACITY

TABLE D-1
SUMMARY OF CO TEST RESULTS

Date	Time	CO, ppm
June 11, 1974	1500 - 1700	15
June 12, 1974	1030 - 1230	580
June 13, 1974	930 - 1130	30

The following graph is the calibration curve for the NDIR Analyzer.

10-2-1970 J.O.T. CH 705
10-2-1970 J.O.T. CH 705
MADE IN U.S.A.
NEUFFEL & EBER CO.



NDIR ANALYZER
CO Collection

Residual Load (in % Full Scale)

APPENDIX E
OPACITY TEST RESULTS

The relative opacity of each of the six stacks was determined by EPA Method 9. The opacity determinations were conducted for two hours on each stack during the particulate tests. Two certified EPA-9 observers read each stack except Stack No. 5, which was read by one observer. The results are summarized in Table E-1.

TABLE E-14
SUMMARY OF OPACITY READINGS: NO. 5 LIME KILN

[illegible]

APPENDIX F
FIELD DATA

Company: Marblehead

Location: Gary, Indiana

Facility: Lime Kiln

Unit No.: 5

Operators:

Date: June 11, 1974

Data Set No.: 1 | Page 2

	Units	1430	1530	1600	1630	1700	1725	1805
Stone Feed Rate	tons/hr	55	55	55	55	55	55	55
Coal Feed Rate	tons/hr	5.75	5.75	5.8	5.8	5.7	5.7	5.7
Bag Collector Press. (Control Room)	in. H ₂ O	2.4	2.3	2.2	2.2	2.1	2.2	0.9
" " " * (Bag House)	in. H ₂ O	1.8	2.0	1.9	1.8	1.8	1.7	1.8
Backend Temp.	°F	—	—	—	—	—	—	—
Calcining Temp	°F	—	—	—	—	—	—	—
Burning Zone Temp	°F	1525	1540	1570	1600	1620	1650	1650
Kiln Draft	-in. H ₂ O	1.4	2.6	2.6	2.6	2.7	2.9	2.8
Hood Draft	in. H ₂ O	-.5	-.4	-.4	-.39	-.42	-.43	-.37
Burner Pressure	in. H ₂ O	4.7	4.7	4.8	4.8	4.8	4.8	4.8
Oxygen	%	2.2	1.6	2.1	3.25 *	1.8	1.7	2.1
Combustibles	%	0	0	0	0	0	0	0
I.D. Fan Temp.	°F	586	560	570	585	585	585	590
Coal Feed Counter	revolutions	990709	991258	991597	991901	992269	992408	992811
Time	24-hour	1430	1527	1602	1633	1701	1726	1808
Stone Feed Counter	revolutions	3254067	3257779	3259913	3261858	3263615	3265184	3267760
Time		1429	1528	1602	1633	1701	1726	1807
I.D. Fan Speed	rpm	620	620	620	620	620	620	620
Primary Air Fan Damper	%	34	34	34	34	34	34	34
Kiln Speed	RPM	64	64	64	64	63.5	63.5	64
Stone Feed Weight Intg.*	100 tons	263461	267298	269180	271126	272820	274452	277151
Time	24-hour	1432	1534	1604	1635	1702	1728	1811
Coal Feed Weight Intg.*	100 tons	092585	093173	093465	093769	094056	094276	094678
Time	24-hour	1432	1533	1603	1634	1704	1727	1809
Baghouse Temp	°F	585	570	575	582	580	580	592

* * Oxygen probe was removed for cleaning during this period. (main probe out) 5%.

Company

Marblehead

Location

Gary, Indiana

Facility

Lime Kiln

Unit No.

5

Operators

Date Jun-12, 1974

Data Set No. 2

Page 1

	Units	930	1015	1100	1130	1200	1230	1300	1330
Stone Feed Rate	tons/hr	58.5	57	55.5	55.5	55.5	55.5	55.5	55.5
Coal Feed Rate	tens/hr	5.6	5.8	5.75	5.6	5.6	5.8	5.8	5.8
Bag Collector Pressure (Control Room)	in. H ₂ O	1.3	1.2	1.1	1.1	1.1	1.1	1.1	1.1
" " (Baghouse)	in. H ₂ O	1.6	1.5	1.2	1.3	1.5	1.5	1.5	1.4
Backend Temp.	°F	—	—	—	—	—	—	—	—
Calcining Temp.	°F	—	—	—	—	—	—	—	—
Burning Zone Temp. ⁸² (81.5° F at P.)	°F	1656	1570	1550	1550	1556	1570	1590	1600
Kiln Draft	-in. H ₂ O	2.9	3.0	2.8	2.8	3.1	3.2	3.2	3.0
Hood Draft	in. H ₂ O	-.5 ⁺	-.5 ⁺	-.5	-.5 ⁺	-.5 ⁺	-.5 ⁺	-.5 ⁺	-.5 ⁺
Burner Pressure	in. H ₂ O	4.5	4.5	4.6	4.6	4.6	4.6	4.6	4.6
Oxygen	%	1.7	2.3	1.9	—*	1.0	1.7	1.7	1.4
Combustibles	%	0	0	0	0	0	0	0	0
I.D. Fan Temp.	°F	560	580	580	580	585	592	600	600
Coal Feed Counter	revolutions	001832	002250	002670	002950	003259	003538	003838	004120
Time	24-hour	933	1017	1100	1129	1207	1231	1302	1331
Stone Feed Counter	revolutions	3327966	3330932	3333683	3335474	3337648	3339572	3341567	3343421
Time	24-hour	931	1016	1058	1127	1201	1231	1302	1331
I.D. Fan Speed	rpm	595	600	540	540	590	590	590	560
Primary Air Fan Position (Dumper Position)	%	34	34.5	35	35	35	35	35	35
Kiln Speed	rph	68	67	66	66	66	66	66	66
Stone Feed Weight Intg.	1/100 tons	337380	340013	343085	344939	347049	348843	350833	352758
Time	24-hour	935	1015	1103	1132	1205	1233	1304	1334
Coal Feed Weight Intg.	1/100 tons	103698	104079	104547	104827	105136	105407	105706	105998
Time	24-hour	934	1014	1102	1131	1204	1232	1303	1333
Baghouse Temp.	°F	550	560	585	582	580	590	600	600

10:00 Stone Feed rate dropped to 55.5 tph.

*O₂ meter off-line (prior O/E of stack).

Company Marblehead Location Gary, Indiana
 Facility Lime Kiln Unit No. 5
 Operators _____ Date June 12, 1974
 _____ Data Set No. 2 | Page 2

	Units	1400	1430	1530	1600				
Stone Feed Rate	tons/hr.	55.5	55.5	55.5	56				
Coal Feed Rate	tons/hr.	5.7	5.8	5.7	5.75				
Bag Collector Press (at id Pass)	in. H ₂ O	1.1	1.1	1.1	1.1				
" " " (Baghouse)	in. H ₂ O	1.5	1.4	1.4	1.4				
Backend Temp.	°F	—	—	—	—				
Caleining Temp.	°F	—	—	—	—				
Burning Zone Temp.	°F	1540	1575	1625	1625				
Kiln Draft	in H ₂ O	3.0	3.1	3.2	3.2				
Hood Draft	in H ₂ O	-.5 ⁺	-.5 ⁺	-.5 ⁺	-.5 ⁺				
Burner Pressure	in H ₂ O	4.7	4.7	4.7	4.7				
Oxygen	%	1.4	—*	1.6	1.9				
Combustibles	%	0	0	0	0				
I.O. Fan Temp	°F	590	595	595	600				
Coal Feed Counter	rev.	004427	004700	005328	005568				
Time	24-hour	1403	1431	1536	1401				
Stone Feed Counter	rev.	3345477	3347277	3351461	3353124				
Time	24-hour	1403	1431	1536	1402				
I.O. Fan Speed	rpm	600	580	580	580				
Primary Air Fan Damper Position	% open	35	35	35	35				
Kiln Speed	rph	66	66	66	66				
Stone Feed Intg.	100 tons	354815	356613	360855	362398				
Time	24-hour	1406	1434	1539	14048				
Coal Feed Intg.	100 tons	106306	106577	107214	107445				
Time	24-hour	1405	1433	1538	1403				
Baghouse Temp.	°F	590	590	595	595				

O₂ level $\approx 0.2\%$ between 11:30-11:45 a

(24 hr ... 24 = 11:30 a) *O₂ meter off-line

Company Marblehead Location Gary, Indiana
 Facility Lime Kiln Unit No. 5
 Operators _____ Date June 13, 1974
 _____ Data Set No. 3 Page 1

	Units	0915	1000	1030	1000	1130	1230	1300	1330
Stone Feed Rate	tons/hr.	52.5	52.5	54	54.5	55.5	55.5	55.5	55.5
Coal Feed Rate	tons/hr.	5.6	5.6	5.6	5.5	5.4	5.5	5.6	5.5
Bag Collector Press. (C. tal. Pn.)	in. H ₂ O	0.8	0.8	0.8	0.8	0.8	0.8	0.8	0.8
" " " (Baghouse)	in. H ₂ O	1.4	1.4	1.4	1.4	1.4	1.4	1.5	1.4
Backend Temp.	°F.	—	—	—	—	—	—	—	—
Calcining Zone Temp	°F	—	—	—	—	—	—	—	—
Burning Zone Temp	°F Blue Tail Pn.	1600	1750	1850	1850	1875	1820	1775	1675
Kiln Draft	-in. H ₂ O	3.2	3.1	3.2	3.2	3.1	3.2	3.2	3.2
Hood Draft	in. H ₂ O	-.5 ⁺	-.5 ⁺	-.5 ⁺	-.5 ⁺	-.5 ⁺	-.5 ⁺	-.5 ⁺	-.5 ⁺
Burner Pressure	in. H ₂ O	6.0	6.0	6.0	6.1	6.0	6.0	6.0	6.0
Oxygen	%	1.4	1.4	1.4	1.5	1.5	1.5	1.6	1.5
Combustibles	%	0	0	0	0	0	0	0	0
I.D. Fan Temp.	°F	600	590	590	585	570	580	580	585
Coal Feed Counter	rev.	0153.52	0157.36	0160.44	0163.00	0165.26	0171.78	0174.00	0177.00
Time	24-hour	0917	0958	1031	1059	1130	1234	1258	1331
Stone Feed Counter	rev.	34184.48	34209.20	34229.81	34247.29	34267.14	34308.75	34324.39	34345.55
Time	24-hour	0917	0958	1031	1059	1130	1234	1258	1331
I.D. Fan Speed	rpm	560	560	560	560	560	560	560	560
Primary Air Fan Damper Position	% open	40	40	40	40	40	40	40	40
Kiln Speed	rph	61.5	61.5	63	64	66	67	67	67
Stone Feed Intg.	% tons	427716	430248	4322.52	43407.2	436053	440151	444522	443835
Time	24-hour	0919	1001	1033	1102	1133	1236	1257	1334
Coal Feed Intg.	% tons	117220	117613	117911	118197	118462	119046	119240	119586
Time	24-hour	0918	1000	1032	1101	1132	1235	1256	1333
Baghouse Temp.	°F	600	590	590	580	560	580	580	580

~ 10 min. Stone rate increased to 54.5 tons. ~ 11:05 a.m. Stone rate went to 55.5 tons

Gary, Indiana

5-

June 13, 1974

3]

Page 2

1) Harshbarger personal feels that these are the most accurate of the feed rate meters.

TRAVERSE POINT LOCATION FOR CIRCULAR DUCTS

PLANT MARBLEHEAD Lime
 DATE JUNE 10, 74
 SAMPLING LOCATION _____
 INSIDE OF FAR WALL TO
 OUTSIDE OF NIPPLE. (DISTANCE A) _____
 INSIDE OF NEAR WALL TO
 OUTSIDE OF NIPPLE. (DISTANCE B) _____
 STACK I.D.. (DISTANCE A - DISTANCE B) _____
 NEAREST UPSTREAM DISTURBANCE _____
 NEAREST DOWNSTREAM DISTURBANCE _____
 CALCULATOR _____

SCHEMATIC OF SAMPLING LOCATION

TRAVERSE POINT NUMBER	FRACTION OF STACK I.D.	STACK I.D.	PRODUCT OF COLUMNS 2 AND 3 (TO NEAREST 1/8 INCH)	DISTANCE B	TRAVERSE POINT LOCATION FROM OUTSIDE OF NIPPLE (SUM OF COLUMNS 4 & 5)
1	1.1	88"	.96		
2	3.2		2.8		
3	5.5		4.8		
4	7.9		6.95		
5	10.5		9.24		
6	13.2		11.6		
7	16.1		14.2		
8	19.7		17.3		
9	23.0		20.2		
10	27.2		23.9		
11	32.3		28.4		
12	39.6		35.0		
13	60.2		53.0		
14	67.7		59.6		
15	72.8		64.1		
16	77.0		67.8		
17	80.6		70.9		
18	83.9		73.8		
19	86.8		76.4		
20	89.5		78.8		
21	92.1		81.0		
22	94.5		83.2		
23	96.8		85.2		
24	98.9		87.0		

MARBLEHEAD Lime Co. 6/10/74

WET-BULB

DRY-BULB

114
116
116
118
118
119
120
118
117
118

156
164
167
175
179
185
187
188
188
188

PRELIMINARY VELOCITY TRAVERSE

PLANT Marblehead Limb
 DATE 6/10/79
 LOCATION Stack 2
 STACK I.D. _____
 BAROMETRIC PRESSURE, in. Hg _____
 STACK GAUGE PRESSURE, in. H₂O _____
 OPERATORS _____

SCHEMATIC OF TRAVERSE POINT LAYOUT

Corrected

TRAVERSE POINT NUMBER	VELOCITY HEAD (Δp_s), in. H ₂ O	STACK TEMPERATURE (T_s), °F
1	.08	255°
2	.12	
3	.12	
4	.13	
5 ^{SE}	.13	
6	.13	
7	.13	
8	.13	
9	.13	
10	.13	
11	.13	
12	.13	
13	.14	
14	.14	
15	.14	
16	.15	
17	.14	
18	.15	
19	.14	
20	.14	
21	.14	
22	.14	
23	.12	
24	.	
AVERAGE		

TRAVERSE POINT NUMBER	VELOCITY HEAD (Δp_s), in. H ₂ O	STACK TEMPERATURE (T_s), °F
.01		
.05		
.05		
.06		
.06		
.06		
.06		
.06		
.06		
.06		
.06		
.06		
.06		
.06		
.07		
.07		
.07		
.07		
.07		
.07		
.07		
.07		
.07		
.07		
.07		
.05		
AVERAGE		

STW INCORPORATED

Field Test Data

Plant Marblehead Lim Co.

Location Gary Ind.

Date June 11, 1974

Run No. 1

Stack No. 1.

Amb. Temp.

Bar. Pressure

Stack Pressure

Nozzle Size $\frac{1}{2}$ "

Heater Box Setting 250

Probe Heater Setting 250

Point Number	Sampling Time (Min)	Stack Temp. of	Velocity Head (ΔP_s)	Pressure Differential Across Meter (ΔH) In. H_2O	Gas Sample Volume Ft^3	Gas Sample Temp. at Dry Gas Meter of	Sample Box Temp. of	Temp. of Gas Impinger Inlet of	Temp. of Gas Impinger Outlet of
Start	1600		$\Delta P, \Delta P_s$		1450.43				
24	05	285	.646	200	1454.0	65	245	—	50
23	10	285	.04	.200	1457.5	65	255	—	50
22	15	290	.04	.20	1461.0	65	260	—	50
21	20	291	.05	.224	1465.0	65	260	—	60
20	25	292	.05	.224	1464.7	70	250	—	60
19	30	290	.05	.224	1472.6	70	275	—	60
18	35	300	.05	.224	1476.5	70	275	—	70
17	40	300	.05	.224	1480.5	80	265	—	75
16	45	300	.05	.224	1484.5	85	270	—	75
15	50	300	.05	.224	1488.5	85	255	—	75
14	55	300	.05	.224	1492.5	85	253	—	80
13	1700	300	.05	.224	1496.5	90	255	—	80
12	05	295	.06	.248	1500.8	95	245	—	80
11	10	300	.06	.245	1504.8	95	250	—	80
10	15	300	.06	.245	1509.2	95	250	—	80
9	20	300	.05	.224	1513.2	100	230	—	70
8	25	300	.05	.224	1517.1	100	230	—	70
7	30	295	.05	.224	1521.0	90	240	—	65
6	35	300	.05	.224	1525.0	100	245	—	60
5	40	300	.05	.224	1529.0	100	255	—	60
4	45	300	.05	.224	1533.0	100	260	—	60
3	50	300	.05	.224	1537.0	100	260	—	60
2	55	270	.04	.200	1541.5	100	260	—	60
1	1800	200	.03	.175	1543.59	100	260	—	
					915.67	= 2000			
					97.16	0.5			
					101.90	150			
					VWP				
Total		6925	5.292	237					
Average		291	.221	0.99	126.3				

PARTICULATE TEST NO. /

I. Total Water Collected

	<u>Silica Gel</u>	<u>Impingers</u>
Final		524
Initial		300
Net	41	224
Total	=	265 ml

II. Conversion of Water Collected to gas at Meter Conditions
(for gas meter internally corrected to 70°F)

$$P_m = P_b + P_o / 13.6 = 29.09 + 0.96 / 13.6$$
$$= 29.16 \text{ in Hg}$$

$$V_v = 1.415 \times \text{ml/Pm} = 1.415 \times 265 / 29.16$$
$$= 12.86 \text{ cu.ft.}$$

III. Percent Moisture of Flue Gas

$$V_v / V_v + V_m = 12.86 / (126.3 + 12.86)$$
$$= 6.5\%$$

199.16

$$\begin{array}{r} 19.916 \\ 0.4 \\ \hline = 22.13 \\ + 199.16 \\ \hline 221.29 \end{array}$$

IV. Relative Density of Flue Gas
From Fyrite Analysis:

CO ₂	=	% Vol, dry
O ₂	=	% Vol, dry
N ₂	=	% Vol, dry

Determination of Average Molecular Weight of Flue Gas

H ₂ O	=	18 x	=
CO ₂	=	44 x	=
O ₂	=	32 x	=
N ₂	=	28 x	=

Relative Flue Gas Density

$$G_d = \quad / 28.95 = \quad$$

PARTICULATE TEST NO.

V. Average Flue Gas Velocity

$$P_s = 29.09 - .04 / 13.6 = 29.09 \text{ in.Hg}$$

$$V_s = 2.9 \times F_s \times \sqrt{\frac{29.92 \times T_s}{P_s \times G_d}} \times \sqrt{P} \text{ avg.}$$

$$= 2.9 \times 0.83 \times \sqrt{\frac{29.92 \times 749}{29.09 \times 1}} \times 2.20$$

$$= \underline{14.7 \text{ ft/sec}}$$

VI. Actual Flue Gas Flowrate

$$V = V_s \times \text{Area} \times 60 = \quad \times \quad \text{Sq.ft.} \times 60$$

$$= \underline{\quad \quad \quad \text{ACFM}}$$

VII. Wet Meter Volume Converted to Stack Conditions

$$MV_m = V_v + V_m = \quad + \quad = 199.16 \text{ cu.ft.}$$

$$MV_s = MV_m \times \frac{P_m}{P_s} \times \frac{T_s}{530} = 199.16 \times \frac{29.16}{29.09} \times \frac{749}{530}$$

$$= \underline{282.13 \text{ cu. ft.}}$$

VIII. Dry Meter Volume Converted to Standard Conditions

$$MV_{std} = V_m \times P_m / 29.92 = 196.3 \times 29.16 / 29.92$$

$$= \underline{181.57 \text{ DSCF}}$$

IX. Weight of Particulate Collected

Gross
Tare

Net

$$D = \text{TOTAL} = \underline{\quad \quad \quad} \text{ grams}$$

PARTICULATE TEST NO.

X. Dust Concentration

$$\begin{aligned}\text{Grains/ACF} &= 15.43 \times D/\text{MVs} = 15.43 \times / \\ &= \underline{\hspace{1cm}} \text{grains/ACF}\end{aligned}$$

$$\begin{aligned}\text{Grains/DSCF} &= 15.43 \times D/\text{MVstd} = 15.43 \times / \\ &= \underline{\hspace{1cm}} \text{grains/DSCF}\end{aligned}$$

XI. Emission Rate

$$\begin{aligned}\text{Pounds/hr} &= D \times V \times 60/\text{MVs} \times 454 \\ &= \quad \times \quad \times 60/ \quad \times 454 \\ &= \quad \text{lb/hr}\end{aligned}$$

$$\begin{aligned}\text{Pounds/Million Btu} &= \quad \text{lb/hr} / \quad \times 10^6 \text{ Btu/hr} \\ &= \underline{\hspace{1cm}} \text{lb/million Btu}\end{aligned}$$

XII. Percent Isokinetic Sampling

$$\begin{aligned}Z &= 305.6 \times \text{MVs}/\text{Vs} \times t \times d^2 \\ &= 305.6 \times 282.3/14.7 \times \frac{140}{100} \times (.5)^2 \\ &= \underline{\underline{97.8}} \%\end{aligned}$$

STW TESTING, INC.

Field Test Data

Plant
Location
Date
Run No.

Stack 2

R_m = 3.54 UH

Amb. Temp.
Bar. Pressure
Stack Pressure
Nozzle Size 1/2
Heater Box Setting 2
Probe Heater Setting

05 = .79
04 = .71
03 = .62
02 :

Traverse Point Number	Sampling Time (Min)	Stack Temp. OF	Velocity Head (AP _s) Pitot	Pressure Differential Across Meter (ΔH) In. H ₂ O	Gas Sample Volume Ft ³	Gas Sample Temp. at Dry Gas Meter OF	Sample Box Temp. OF	Temp. of Gas Impinger Inlet OF	Temp. of Gas Impinger Outlet OF
Start	6:01	260	.03	.173	1521.52	60	210		50
1	06	263	.03	.173	1524.3	60	210		50
2	11	260	.03	.173	1528.7	60	250		50
3	16	260	.04	.200	1530.0	60	235		50
4	21	260	.03	.173	1533.7	65	220		55
5	26	250	.03	.173	1536.5	60	220		50
6	31	260	.05	.224	1540.7	70	225		55
7	36	260	.03	.173	1544.9	70	240		60
8	41	270	.05	.224	1547.7	80	240		60
9	46	260	.05	.224	1551.6	80	250		65
10	51	270	.04	.200	1555.2	80	255		65
11	56	260	.04	.200	1558.6	85	260		70
12	17:01	260	.03	.173	1562.0	85	260		70
13	06	260	.04	.200	1565.3	90	250		65
14	11	275	.04	.200	1568.4	90	250		65
15	16	260	.04	.200	1572.2	90	250		70
16	21	275	.04	.200	1575.7	95	260		70
17	26	275	.05	.224	1579.6	95	260		70
18	31	260	.05	.224	1583.3	100	265		60
19	36	250	.04	.200	1586.7	90	265		60
20	41	260	.03	.173	1590.0	95	265		60
21	46	270	.03	.173	1593.2	95	265		60
22	51	260	.03	.173	1595.4	95	265		60
23	56	260	.03	.173	1599.2	100	260		60
24	18:01	240	.04	.200	1602.49	95	260		60
should be 82.4					80.77	102.70 150			
VAP			4.65	16.97	166.93				
Total									
Average		263	.194						

PARTICULATE TEST NO.

I. Total Water Collected

	<u>Silica Gel</u>	<u>Impingers</u>
Final		452
Initial		300
Net	21	152
Total	=	173 ml

II. Conversion of Water Collected to gas at Meter Conditions
(for gas meter internally corrected to 70°F)

$$P_m = P_b + P_o/13.6 = 29.09 + 0.76/13.6 \\ = 29.15 \text{ in Hg}$$

$$V_v = 1.415 \times \text{ml}/P_m = 1.415 \times 173/29.15 \\ = \underline{8.40} \text{ cu. ft.}$$

III. Percent Moisture of Flue Gas

$$V_v/(V_v + V_m) = 8.40/(8.40 + 166.98) \\ = \underline{4.8\%}$$

175.38

$$.10 = x/(x + 166.98)$$

IV. Relative Density of Flue Gas
From Fyrite Analysis:

CO ₂	=	% Vol, dry
O ₂	=	% Vol, dry
N ₂	=	% Vol, dry

$$.10x + 16.698 = x$$

$$16.698 = 0.9x$$

$$18.55 = x$$

$$+ 166.98$$

$$\underline{185.53}$$

Determination of Average Molecular Weight of Flue Gas

H ₂ O	=	18 x	=
CO ₂	=	44 x	x
O ₂	=	32 x	x
N ₂	=	28 x	x

Relative Flue Gas Density

$$G_d = \quad /28.95 = \underline{\hspace{2cm}}$$

PARTICULATE TEST NO.

V. Average Flue Gas Velocity

$$P_s = 29.07 - .04/13.6 = 29.07 \text{ in.Hg}$$

$$V_s = 2.9 \times F_s \times \sqrt{\frac{29.92 \times T_s}{P_s \times G_d}} \times \sqrt{P \text{ avg.}}$$

$$= 2.9 \times 0.83 \times \sqrt{\frac{29.92 \times 723}{29.07 \times 1.0}} \times 0.197$$

$$= \underline{13.1 \text{ ft/sec}}$$

$$\sqrt{743.6} = 27.27$$

VI. Actual Flue Gas Flowrate

$$V = V_s \times \text{Area} \times 60 = \quad \times \quad \text{Sq.ft.} \times 60$$
$$= \underline{\text{ACFM}}$$

VII. Wet Meter Volume Converted to Stack Conditions

$$MV_m = V_v + V_m = \quad + \quad = \quad \text{cu.ft.}$$

$$MV_s = MV_m \times \frac{P_m}{P_s} \times \frac{T_s}{530} = 175.38 \times \frac{29.15}{29.07} \times \frac{723}{530}$$

$$= \underline{240.40 \text{ cu. ft.}}$$

VIII. Dry Meter Volume Converted to Standard Conditions

$$MV_{std} = V_m \times \frac{P_m}{29.92} = \quad \times \quad /29.92$$

$$= \underline{\text{DSCF}}$$

IX. Weight of Particulate Collected

Gross
Tare

Net

$$D = \text{TOTAL} = \underline{\quad\quad\quad} \text{ grams}$$

PARTICULATE TEST NO.

X. Dust Concentration

$$\begin{aligned}\text{Grains/ACF} &= 15.43 \times D/\text{MVs} = 15.43 \times / \\ &= \underline{\hspace{2cm}} \text{grains/ACF}\end{aligned}$$

$$\begin{aligned}\text{Grains/DSCF} &= 15.43 \times D/\text{MVstd} = 15.43 \times / \\ &= \underline{\hspace{2cm}} \text{grains/DSCF}\end{aligned}$$

XI. Emission Rate

$$\begin{aligned}\text{Pounds/Hr} &= D \times V \times 60/\text{MVs} \times 454 \\ &= \quad \times \quad \times 60/ \quad \times 454 \\ &= \quad \text{lb/hr}\end{aligned}$$

$$\begin{aligned}\text{Pounds/Million Btu} &= \quad \text{lb/hr} / \quad \times 10^6 \text{ Btu/hr} \\ &= \underline{\hspace{2cm}} \text{lb/million Btu}\end{aligned}$$

XII. Percent Isokinetic Sampling

$$\begin{aligned}\% &= 305.6 \times \text{MVs} (\text{Vs} \times t \times d^2) \\ &= 305.6 \times 240.4/13.1 \times 240 \times (.5)^2 \\ &= \underline{93.5} \%\end{aligned}$$

Field Test Data

Plant Marblehead Lime Co
Location Cory Indus
Date 6/12/74
Run No.

54266. 3

$$R_m = 3,68 \sqrt{H}$$

Amb. Temp.

Bar. Pressure 29.21

Stack Pressure

Nozzle Size $\frac{1}{2}$ " diameter

Heater Box Setting 3.20

Probe Heater Setting 25°C

[illegible]

Field Test Data

5f2-k43

$$R_{un} = 3.68 \sqrt{H}$$

Amb. Temp. 75°F
Bar. Pressure 29.22
Stack Pressure
Nozzle Size 1/2" d. zinc
Heater Box Setting 250
Probe Heater Setting 250

[illegible]

PARTICULATE TEST NO.

I. Total Water Collected

	<u>Silica Gel</u>	<u>Impingers</u>
Final		500
Initial		300 500
Net	32.0	
Total	=	ml

II. Conversion of Water Collected to gas at Meter Conditions
(for gas meter internally corrected to 70°F)

$$P_m = P_b + (P_o/13.6) = \quad + \quad /13.6$$

= in Hg

$$V_v = 1.415 \times \text{ml}/P_m = 1.415 \times \quad /$$

= cu.ft.

III. Percent Moisture of Flue Gas

$$V_v/(V_v + V_m) = \quad / \quad +$$

= %

IV. Relative Density of Flue Gas
From Fyrite Analysis:

CO ₂	=	% Vol, dry
O ₂	=	% Vol, dry
N ₂	=	% Vol, dry

Determination of Average Molecular Weight of Flue Gas

H ₂ O	=	18 x	=
CO ₂	=	44 x	x =
O ₂	=	32 x	x =
N ₂	=	28 x	x = <u> </u>

Relative Flue Gas Density

$$G_d = \quad /28.95 = \quad$$

6-7-77

Plant
Location
Date
Run No.
North
Rm : 3.68 $\sqrt{N}$

Amb. Temp. 71°F
Bar. Pressure 29.22
Stack Pressure
Nozzle Size $\rightarrow \frac{1}{2}"$
Heater Box Setting
Probe Heater Setting

[illegible]

PARTICULATE TEST NO.

I. Total Water Collected

	<u>Silica Gel</u>	<u>Impingers</u>
Final		559
Initial		<u>~300</u>
Net	<u>27.0</u>	<u>259</u>
Total	= ml	

II. Conversion of Water Collected to gas at Meter Conditions
(for gas meter internally corrected to 70°F)

$$P_m = P_b + \left(\frac{P_o}{13.6} \right) = \quad + \quad / 13.6$$

in Hg

$$V_v = 1.415 \times \text{ml}/P_m = 1.415 \times \quad /$$

= cu.ft.

III. Percent Moisture of Flue Gas

$$V_v / (V_v + V_m) = \quad / \quad +$$

= %

IV. Relative Density of Flue Gas
From Fyrite Analysis:

CO ₂	=	% Vol, dry
O ₂	=	% Vol, dry
N ₂	=	% Vol, dry

Determination of Average Molecular Weight of Flue Gas

H ₂ O	=	18 x	=
CO ₂	=	44 x	x
O ₂	=	32 x	x
N ₂	=	28 x	x

Relative Flue Gas Density

$$G_d = \quad / 28.95 = \quad$$

STW TESTING, INC.

Field Test Data

Plant Mobile *hwy*

Location

Date 6-13-74

Run No.

Stack 5
North Port

R = 3.64

045: .77

.03 = .82

.055 = .87

.06 = .89

.065 = .93

Amb. Temp. 73 °F

Bar. Pressure 29.21

Stack Pressure

Nozzle Size 0.5

Heater Box Setting

Probe Heater Setting

Traverse Point Number	Sampling Time (Min)	Stack Temp. of	Velocity Head (AP _s)	Pressure Differential Across Meter (ΔH) In. H ₂ O	Gas Sample Volume Ft ³	Gas Sample Temp. at Dry Gas Meter Inlet/Outlet	Sample Box Temp. of	Temp. of Gas Impinger Inlet of	Temp. of Gas Impinger Outlet of
Start	9:35				1719.6				
1	35	280	.055	1.25	1721.9	70	235		55
2	40	280	.06	1.20	1726.3	70	220		55
3	45	280	.06	1.32	1730.8	75	225		55
4	50	280	.05	1.22	1734.7	75	240		60
5	55	280	.055	1.32	1739.0	80	240		60
6	10:00	280	.065	1.52	1743.6	85	250		60
7	105	280	.065	1.55	1748.3	90	260		60
8	110	280	.065	1.55	1752.9	90	240		60
9	115	280	.055	1.32	1757.3	90	245		60
10	120	280	.06	1.45	1761.7	95	250		60
11	125	280	.06	1.47	1766.2	95	250		60
12	130	280	.06	1.47	1770.7	100	245		60
13	135	280	.065	1.80	1774.4	95	240		60
14	140	280	.060	1.90	1777.9	100	240		60
15	145	280	.040	1.90	1781.6	100	245		60
16	150	280	.05	1.22	1785.6	100	245		60
17	155	280	.045	1.022	1789.6	100	245		65
18	11:00	280	.045	1.1	1793.3	100	250		65
19	105	280	.045	.98	1797.1	100	250		65
20	110	280	.045	1.0	1800.2	100	250		60
21	115	280	.045	1.03	1804.7	100	250		60
22	120	280	.05	1.30	1808.9	100	250		60
23	125	277	.04	1.02	1812.7	100	250		60
24	130	270	.045	1.70	1816.4	100	260		65
Total									
Average									

* Run @ 72/min + should be 77/min

STW TESTING, INC.

Field Test Data

Plant *Marblehead*
 Location *G-1, Inc*
 Date *6-13-74*
 Run No. *Stack 5*
South Port

.045 = .77
.05 = .82
.055 = .87
.06 = .89
.065 = .93
.04 = .73
.025 = .50

.075 = 1 Amb. Temp. *76*
.07 = .96 Bar. Pressure *29.17*
 Stack Pressure
 Nozzle Size *.5"*
 Heater Box Setting
 Probe Heater Setting

R = 3645H

Traverse Point Number	Sampling Time (Min)	Stack Temp. OF	Velocity Head (AP _s)	Pressure Differential Across Meter (ΔH) In. H ₂ O	Gas Sample Volume Ft ³	Gas Sample Temp. at Dry Gas Meter OF	Sample Box Temp. OF	Temp. of Gas Impinger Inlet OF	Temp. of Gas Impinger Outlet OF
<i>Start</i>	<i>12.00</i>				<i>1011.03</i>				
<i>1</i>	<i>05</i>	<i>280</i>	<i>.045</i>	<i>.98</i>	<i>1820.5</i>	<i>95</i>	<i>270</i>	<i>70</i>	
<i>2</i>	<i>10</i>	<i>280</i>	<i>.045</i>	<i>.98</i>	<i>1824.3</i>	<i>95</i>	<i>275</i>	<i>60</i>	
<i>3</i>	<i>15</i>	<i>285</i>	<i>.045</i>	<i>1.0</i>	<i>1827.1</i>	<i>95</i>	<i>280</i>	<i>60</i>	
<i>* 4</i>	<i>20</i>	<i>285</i>	<i>.035</i>	<i>-</i>	<i>1833.2</i>	<i>95</i>	<i>280</i>	<i>60</i>	
<i>5</i>	<i>35</i>	<i>280</i>	<i>.03</i>	<i>1.45</i>	<i>1836.7</i>	<i>100</i>	<i>280</i>	<i>60</i>	
<i>6</i>	<i>45</i>	<i>280</i>	<i>.075</i>	<i>1.75</i>	<i>1841.1</i>	<i>95</i>	<i>280</i>	<i>60</i>	
<i>7</i>	<i>55</i>	<i>280</i>	<i>.075</i>	<i>1.8</i>	<i>1846.1</i>	<i>95</i>	<i>270</i>	<i>60</i>	
<i>8</i>	<i>55</i>	<i>280</i>	<i>.070</i>	<i>1.65</i>	<i>1850.0</i>	<i>95</i>	<i>270</i>	<i>60</i>	
<i>9</i>	<i>13.00</i>	<i>275</i>	<i>1.0</i>	<i>1.67</i>	<i>1855.6</i>	<i>100</i>	<i>290</i>	<i>60</i>	
<i>10</i>	<i>15</i>	<i>275</i>	<i>.065</i>	<i>1.52</i>	<i>1860.2</i>	<i>100</i>	<i>300</i>	<i>60</i>	
<i>11</i>	<i>110</i>	<i>275</i>	<i>.065</i>	<i>1.52</i>	<i>1864.7</i>	<i>100</i>	<i>290</i>	<i>60</i>	
<i>12</i>	<i>15</i>	<i>280</i>	<i>.065</i>	<i>1.52</i>	<i>1869.3</i>	<i>100</i>	<i>270</i>	<i>60</i>	
<i>13</i>	<i>20</i>	<i>280</i>	<i>.065</i>	<i>1.52</i>	<i>1874.2</i>	<i>100</i>	<i>280</i>	<i>60</i>	
<i>14</i>	<i>25</i>	<i>280</i>	<i>.065</i>	<i>1.52</i>	<i>1878.4</i>	<i>100</i>	<i>290</i>	<i>60</i>	
<i>15</i>	<i>30</i>	<i>280</i>	<i>.045</i>	<i>.82</i>	<i>1881.9</i>	<i>100</i>	<i>295</i>	<i>60</i>	
<i>16</i>	<i>35</i>	<i>280</i>	<i>.040</i>	<i>.95</i>	<i>1885.3</i>	<i>100</i>	<i>290</i>	<i>65</i>	
<i>17</i>	<i>40</i>	<i>280</i>	<i>.045</i>	<i>.90</i>	<i>1889.1</i>	<i>100</i>	<i>290</i>	<i>65</i>	
<i>18</i>	<i>45</i>	<i>280</i>	<i>.085</i>	<i>1.60</i>	<i>1893.4</i>	<i>105</i>	<i>290</i>	<i>70</i>	
<i>19</i>	<i>50</i>	<i>280</i>	<i>.070</i>	<i>1.75</i>	<i>1898.3</i>	<i>105</i>	<i>290</i>	<i>70</i>	
<i>20</i>	<i>55</i>	<i>280</i>	<i>.045</i>	<i>1.10</i>	<i>1902.2</i>	<i>110</i>	<i>290</i>	<i>65</i>	
<i>21</i>	<i>14.00</i>	<i>245</i>	<i>.045</i>	<i>1.05</i>	<i>1906</i>	<i>110</i>	<i>270</i>	<i>65</i>	
<i>22</i>	<i>14.05</i>	<i>230</i>	<i>.025</i>	<i>1.1</i>	<i>1908.8</i>	<i>110</i>	<i>265</i>	<i>65</i>	
<i>23</i>	<i>10</i>	<i>160</i>	<i>.025</i>	<i>1.05</i>	<i>1911.7</i>	<i>110</i>	<i>270</i>	<i>65</i>	
<i>24</i>	<i>15</i>	<i>110</i>	<i>.02</i>	<i>.5</i>	<i>1914.7</i>	<i>110</i>	<i>270</i>	<i>65</i>	
Total									
Average									

* Fell off level

PARTICULATE TEST NO.

I. Total Water Collected

	<u>Silica Gel</u>	<u>Impingers</u>
Final	390.8	589
Initial	352.8	300
Net	38.0	289
Total	= ml	

II. Conversion of Water Collected to gas at Meter Conditions
(for gas meter internally corrected to 70°F)

$$P_m = P_b + \left(P_o / 13.6 \right) = \quad + \quad / 13.6$$

= in Hg

$$V_v = 1.415 \times \text{ml} / P_m = 1.415 \times \quad /$$

= cu. ft.

III. Percent Moisture of Flue Gas

$$V_v / (V_v + V_m) = \quad / \quad +$$

= %

IV. Relative Density of Flue Gas
From Fyrite Analysis:

CO ₂	=	% Vol, dry
O ₂	=	% Vol, dry
N ₂	=	% Vol, dry

Determination of Average Molecular Weight of Flue Gas

H ₂ O	=	18 x	=
CO ₂	=	44 x	x
O ₂	=	32 x	x
N ₂	=	28 x	x

Relative Flue Gas Density

$$G_d = \quad / 28.95 = \quad$$

STW TESTING, INC.

Field Test Data

Plant Marblehead Lime Co.
 Location Gary, Ind
 Date 6/13/74
 Run No.

Stack #6

Amb. Temp. 73°F
 Bar. Pressure 29.21
 Stack Pressure 29.21
 Nozzle Size 1/2" diam.
 Heater Box Setting 250
 Probe Heater Setting 250

North Port

Rm = 3.6474

Traverse Point Number	Sampling Time (Min)	Stack Temp. OF	Velocity Head (AP _s)	Pressure Differential Across Meter (ΔH) In. H ₂ O	Gas Sample Volume Ft ³	Gas Sample Temp. at Dry Gas Meter OF	Sample Box Temp. OF	Temp. of Gas Impinger Inlet OF	Temp. of Gas Impinger Outlet OF
Start	925				1790.12				
24	30	270.05	.024	1.05	1794.2	70	260	—	70
23	35	270.05	.024	1.00	1798.4	75	260	—	60
22	40	270.06	.024	1.20	1802.2	75	260	—	65
21	45	270.06	.024	1.30	1807.1	80	250	—	70
20	50	270.06	.024	1.30	1811.6	80	255	—	70
19	55	270.06	.024	1.30	1816.1	85	250	—	70
18	1000	275.05	.024	1.15	1820.2	90	275	—	70
17	05	270.05	.024	1.15	1824.0	90	270	—	65
16	10	275.05	.024	1.20	1828.4	90	245	—	65
15	15	250.05	.024	1.20	1832.8	95	255	—	60
14	20	275.05	.024	1.20	1837.0	90	255	—	65
13	25	275.05	.010	1.00	1840.8	95	255	—	65
12	30	270.05	.024	1.20	1845.0	95	250	—	65
11	35	270.05	.024	1.20	1849.3	100	245	—	65
10	40	270.05	.024	1.2	1853.4	100	245	—	70
9	45	270.05	.024	1.2	1857.7	100	250	—	70
8	50	260.05	.024	1.2	1861.8	100	250	—	65
7	55	260.05	.024	1.2	1866.0	100	250	—	65
6	1100	265.04	.2	1.0	1869.7	100	250	—	60
5	05	260.03	.173	0.8	1872.5	100	250	—	60
4	10	260.03	.173	0.8	1876.6	100	250	—	60
3	15	260.03	.173	0.8	1879.8	100	250	—	65
2	20	260.03	.141	0.6	1882.5	100	250	—	65
1	25	255.02	.141	0.5	1885.13	100	250	—	65
Total									
Average									

6/13/74

२२९

Field Test Data

Plant MARBLEHEAD Lime Co.

Location Gary Ind.

Date 6/3/74

~~Rev. No.~~

5202-56

South Port

$$P_m = 3.64 \sqrt{H}$$

Amb. Temp. 73° F.

Bar. Pressure 29.21

Stack Pressure 29.21

Nozzle Size 0.5" dia.

Heater Box Setting 25-25

Probe Heater Setting 2.5×10^3

[illegible]

PARTICULATE TEST NO.

I. Total Water Collected

	<u>Silica Gel</u>	<u>Impingers</u>
Final	390.3	529
Initial	352.8	300
	<u>37.5</u>	<u>229</u>
Net		
Total	= _____ ml	

II. Conversion of Water Collected to gas at Meter Conditions
(for gas meter internally corrected to 70°F)

$$P_m = P_b + \left(\frac{P_o}{13.6} \right) = \quad + \quad / 13.6$$

= in Hg

$$V_v = 1.415 \times \text{ml}/P_m = 1.415 \times \quad /$$

= _____ cu.ft.

III. Percent Moisture of Flue Gas

$$V_v / (V_v + V_m) = \quad / \quad +$$

= _____ %

IV. Relative Density of Flue Gas
From Fyrite Analysis:

CO ₂	=	% Vol, dry
O ₂	=	% Vol, dry
N ₂	=	% Vol, dry

Determination of Average Molecular Weight of Flue Gas

H ₂ O	=	18 x		=
CO ₂	=	44 x	x	=
O ₂	=	32 x	x	=
N ₂	=	28 x	x	= _____

Relative Flue Gas Density

$$G_d = \quad / 28.95 = \quad$$

DRY MOLECULAR WEIGHT DETERMINATION

PLANT Marblehead Lime
 DATE 6/11/74
 SAMPLING TIME (24-hr CLOCK) 10:30-1:30
 SAMPLING LOCATION Stack No. 6 (North)
 SAMPLE TYPE (BAG, INTEGRATED, CONTINUOUS) bag
 ANALYTICAL METHOD Orsat / FYRITE
 AMBIENT TEMPERATURE 65-70°F
 OPERATOR L.K.

COMMENTS:

RUN GAS	1		2		3		AVERAGE NET VOLUME	MULTIPLIER	MOLECULAR WEIGHT OF STACK GAS (DRY BASIS) M _d , lb/lb-mole
	ACTUAL READING	NET	ACTUAL READING	NET	ACTUAL READING	NET			
CO ₂	6.8		6.8		6.7		6.8	44/100	
O ₂ (NET IS ACTUAL O ₂ READING MINUS ACTUAL CO ₂ READING)	could not be read on Orsat		Orsat, required fyrites				19.5	32/100	
CO (NET IS ACTUAL CO READING MINUS ACTUAL O ₂ READING)	unknown							28/100	
N ₂ (NET IS 100 MINUS ACTUAL CO READING)								28/100	
TOTAL									

fyrites

DRY MOLECULAR WEIGHT DETERMINATION

COMMENTS:

PLANT MARBLEHEAD Lime
 DATE 6/12/74
 SAMPLING TIME (24-hr CLOCK) _____
 SAMPLING LOCATION _____
 SAMPLE TYPE (BAG, INTEGRATED, CONTINUOUS) _____
 ANALYTICAL METHOD FRITES
 AMBIENT TEMPERATURE _____
 OPERATOR _____

RUN GAS	1		2		3		AVERAGE NET VOLUME	MULTIPLIER	MOLECULAR WEIGHT OF STACK GAS (DRY BASIS) M _d , lb/lb-mole
	ACTUAL READING	NET	ACTUAL READING	NET	ACTUAL READING	NET			
CO ₂		7.0		7.2		6.8	7.0	44/100	
O ₂ (NET IS ACTUAL O ₂ READING MINUS ACTUAL CO ₂ READING)		16.5		16.0		17.0	16.5	32/100	
CO (NET IS ACTUAL CO READING MINUS ACTUAL O ₂ READING)								28/100	
N ₂ (NET IS 100 MINUS ACTUAL CO READING)								28/100	
TOTAL									

DRY MOLECULAR WEIGHT DETERMINATION

PLANT MARBLEHEAD Lime Co
 DATE 6/13/74
 SAMPLING TIME (24-hr CLOCK) _____
 SAMPLING LOCATION _____
 SAMPLE TYPE (BAG, INTEGRATED, CONTINUOUS) _____
 ANALYTICAL METHOD FYRITES
 AMBIENT TEMPERATURE _____
 OPERATOR _____

COMMENTS:

RUN GAS	1		2		3		AVERAGE NET VOLUME	MULTIPLIER	MOLECULAR WEIGHT OF STACK GAS (DRY BASIS) M_d , lb/lb-mole
	ACTUAL READING	NET	ACTUAL READING	NET	ACTUAL READING	NET			
CO ₂		7.0		7.0		7.0	7.0	44/100	
O ₂ (NET IS ACTUAL O ₂ READING MINUS ACTUAL CO ₂ READING)		16.5		16.5		16.5	16.5	32/100	
CO (NET IS ACTUAL CO READING MINUS ACTUAL O ₂ READING)								28/100	
N ₂ (NET IS 100 MINUS ACTUAL CO READING)								28/100	
TOTAL									

Test Site MARBLEHEAD LYMEDate 11 JUNE 1974Time 12:30Sample No. ONESampling Location STACK NO. 5Sampling Train SO₂Pump Temp. (°F) i 68°
f _____Sampling Rate, l/min 1.0Sampling Time (min) 75% CO₂ _____ ml H₂O _____ Stack Temp. (°F) _____% O₂ _____ Vol. Sampled (l) _____% CO _____ % H₂O _____

Sample No. _____

Sampling Train _____

Time (min)	Sampling Rate (l/min)	Temp. °F	ΔP"	Dry Test Meter (A ³)
0	1.0	68	2.5	127.52
5	1.0	70	2.5	127.70
10	1.0	70	2.5	127.90
15	1.0	70	2.5	128.10
20	0.9	70	2.5	128.30
25	1.1	71	2.5	128.52
30	0.7	73	2.5	128.71

Test Site MARBLEHEAD LIMEDate 11 JUNE 1974

Time _____

Sample No. ONESampling Location STACK NO. 5Sampling Train SO₂Pump Temp. (°F) i 72°

f _____

Sampling Rate, l/min 1.0Sampling Time (min) 25% CO₂ _____ ml H₂O _____ Stack Temp. (°F) _____% O₂ _____ Vol. Sampled (l) _____% CO _____ % H₂O _____

Sample No. _____

Sampling Train _____

Time (min)	Sampling Rate (l/min)	Temp. °F	ΔP"	Dry Test Meter (A ³)
35	1.0	72	2.5	128.92
07 PM 5	1.0	72	2.5	129.01 ← STOP/
10 PM 10	1.0	72	2.5	129.01 (power)
45	1.0	73	2.5	129.21 (LOSS)
17 PM 50	1.0	73	2.5	129.30 ← STOP *
18 PM 50	1.0	73	2.5	129.30 START
50	1.0	73	2.5	129.39
21 PM 55	1.0	73	2.5	129.44 ← STOP
28 PM 60	1.0	73	2.5	129.44 ← START
30 PM 60	1.0	73	2.5	129.55
32 PM	1.0	73	2.5	129.60 ← END

* CO₂ NOT STOPPED HERE. 710

Test Site HAZSLT AD LINEDate 11 JUNE 1974Time 2:00Sample No. TWCSampling Location STACK #5Sampling Train SO₂Pump Temp. (°F) i f Sampling Rate, l/min 1.0Sampling Time (min) 30NOTE: SMOKE FROM CEMENT
FACTORY COMES THE WAY
WINDS ABOUT 20 MPH.% CO₂ ml H₂O Stack Temp. (°F) 270% O₂ Vol. Sampled (l) % CO % H₂O Sample No. Sampling Train NOTE: TEST STARTED AFTER
30 MIN BECAUSE FIRST
IMPINGER WASHING TOX HIGH.

	Time (min)	Sampling Rate (l/min)	Temp. °F	ΔP"	Dry Test Meter (A ³)
2:00 PM	0	1.0	73	2.5	129.69
2:05 PM	5	1.0	75	2.5	129.81
2:10 PM	10	1.0	78	2.5	130.01
2:15 PM	15	1.0	76	2.5	130.21
2:20 PM	20	1.0	77	2.5	130.42
2:25 PM	25	1.0	77	2.5	130.62
2:30 PM	30	1.0	74	2.5	130.83

Test Site MARBLEHEAD LIMEDate 12 JUNE 1974Time 11:00 AMSample No. THREESampling Location STACK NO. 2Sampling Train SO₂Pump Temp. (°F) i 71f Sampling Rate, l/min 1.0Sampling Time (min) % CO₂ ml H₂O Stack Temp. (°F) 280% O₂ Vol. Sampled (l) % CO % H₂O Sample No. Sampling Train

Time (min)	Sampling Rate (l/min)	Temp. °F	ΔP"	Dry Test Meter (A ³)
11:00 AM 0	1.0	71	2.5	130.91
11:05 AM 5	1.0	72	2.5	131.09
11:10 AM 10	1.0	73	2.5	131.30
11:15 AM 15	1.0	73	2.5	131.51
11:20 AM 20	1.0	74	2.5	131.72
11:25 AM 25	1.0	73	2.5	131.96
11:30 30	1.0	75	2.5	132.16

Test Site MARBLEHEAD LIMEDate 12 JUNE 1979Time 11:30 AMSample No. THREESampling Location STACK No. 2Sampling Train SO₂Pump Temp. (°F) i 75f Sampling Rate, l/min 1.0Sampling Time (min) % CO₂ ml H₂O Stack Temp. (°F) 280% O₂ Vol. Sampled (l) % CO % H₂O Sample No. Sampling Train

Time (min)	Sampling Rate (l/min)	Temp. °F	ΔP"	Dry Test Meter (A ³)
30				
35	1.0	72	2.5	132.33
40	1.0	74	2.5	132.54
45				
50				
55				
60				

Test Site MARBLEHEAD LIMEDate 12 JUNE 1979Time 1:50 PMSample No. FOURSampling Location STACK NO. 2Sampling Train SO₂Pump Temp. (°F) i 72f Sampling Rate, l/min 1.0Sampling Time (min) % CO₂ mℓ H₂O Stack Temp. (°F) % O₂ Vol. Sampled (ℓ) % CO % H₂O Sample No. Sampling Train

Time (min)	Sampling Rate (ℓ/min)	Temp. °F	ΔP"	Dry Test Meter (A ³)
1:50 PM 0	1.0	72	2.5	132.83
1:55 PM 5	1.0	73	2.5	133.09
2:00 PM 10	1.0	75	2.5	133.25
2:05 PM 15	1.0	77	2.5	133.45
2:10 PM 20	0.9	81	2.5	
2:15 PM 25	1.0	81	2.5	133.85
2:20 30	1.1	83	2.5	134.07

Test Site MARBLEHEAD LIMEDate 12 JUNE 1974Time 2:25 PMSample No. FOURSampling Location STACK NO. 2Sampling Train SO₂Pump Temp. (°F) i 81f Sampling Rate, l/min 1.0Sampling Time (min) % CO₂ ml H₂O Stack Temp. (°F) % O₂ Vol. Sampled (l) % CO % H₂O Sample No. Sampling Train

Time (min)	Sampling Rate (l/min)	Temp. °F	ΔP"	Dry Test Meter (A ³)
0				
2:25 PM 35	1.0	81	2.5	134.26
2:30 PM 40	0.8	81	2.5	134.45
45				
50				
55				
60				

NOTE: SAMPLING STOPPED AFTER 40 MIN BECAUSE
FIRST IMPINGER (ISOPROPAL) BUBBLING TOO
HIGH.

Test Site MARBLEHEAD LIMEDate 13 JUNE 1974Time 9:25 AMSample No. FIVESampling Location STACK NO. 2Sampling Train SO₂Pump Temp. (°F) i f Sampling Rate, l/min 1.0Sampling Time (min) 40% CO₂ ml H₂O Stack Temp. (°F) 280% O₂ Vol. Sampled (l) % CO % H₂O Sample No. Sampling Train

Time (min)	Sampling Rate (l/min)	Temp. °F	ΔP"	Dry Test Meter (A ³)
9:25 AM 0	1.0	72	2.5	139.82
9:30 AM 5	1.0	73	2.5	135.03
9:35 AM 10	1.0	76	2.5	135.23
9:40 AM 15	1.0	78	2.5	135.44
9:45 AM 20	1.0	80	2.5	135.66
9:50 AM 25	1.0	83	2.5	135.875
9:55 AM 30	1.0	85	2.5	136.09

Test Site MARBLEHEAD LIMEDate 13 JUNE 1974Time 10:00 AMSample No. FIVESampling Location STACK NO. 2Sampling Train SO₂Pump Temp. (°F) i 85f Sampling Rate, l/min 1.0Sampling Time (min) 40

NOTE: AGAIN TEST CONCLUDED

DUE TO EXCESSIVE
BUBBLING OF ISOPROPYNOX
IN IMPINGER #1% CO₂ ml H₂O Stack Temp. (°F) 280% O₂ Vol. Sampled (l) % CO % H₂O Sample No. Sampling Train

Time (min)	Sampling Rate (l/min)	Temp. °F	ΔP"	Dry Test Meter (A ³)
0				
10:00 AM <u>35</u>	<u>0.95</u>	<u>88</u>	<u>2.5</u>	<u>136.29</u>
10:05 AM <u>40</u>	<u>1.0</u>	<u>88</u>	<u>2.5</u>	<u>136.51</u> STOP.
<u>45</u>				
<u>20</u>				
<u>25</u>				
<u>30</u>				

40 ~~5~~ min

Test Site MARBLEHEAD LIMEDate 13 JUNE 1974Time 10:42 AMSample No. SIXSampling Location STACK NO. 2Sampling Train SO₂Pump Temp. (°F) i
f Sampling Rate, l/min 1.0Sampling Time (min) NOTE: SAMPLING STOPPED DUE
TO EXCESSIVE BUBBLING
IN FIRST IMPINGER.% CO₂ mL H₂O Stack Temp. (°F) 275% O₂ Vol. Sampled (L) % CO % H₂O Sample No. Sampling Train

Time (min)	Sampling Rate (l/min)	Temp. °F	ΔP"	Dry Test Meter (A ³)
10:42 AM 0	1.0	78	2.5	136.96
10:47 AM 5	1.0	83	2.5	137.17
10:52 AM 10	1.0	84	2.5	137.38
10:57 AM 15	1.0	85	2.5	137.60
11:02 AM 20	1.0	86	2.5	137.82
11:07 AM 25	1.0	87	2.5	138.04
30				

STOP.

25 min

STW INCORPORATED

NO. DATA SHEET

Customer: MARBLE HEAD LIMFCO

Installation: BUFFINGTON

Location: STACK #5, SOUTH PORT

Job No.:

Rate:

8 pipe was 34 inches in diam
inside of stack

Test No.: 1

Amb. Temp:

Test Date: 6-11-74

Test By: D.G. Waden

6/12/74

11:00-11:30 am

Sample Number	Date	Time	Flask Number	Volume of Flask, ml	Initial Conditions			Final Conditions		
					Bar. Press. in. Hg	Flask Temp. of	Flask Vac. in. Hg	Bar. Press. in. Hg	Flask Temp. of	Flask Vac. in. Hg
① A-N-1-1	6-11-74	13:21	7	2038	29.09	72	-27.2	29.21	76	+0.2
② A-N-1-2	6-11-74	14:03	8	2030	29.09	70	-27.2	29.21	74	-0.7
③ A-N-2-1	6-11-74	16:25	9	1961	29.09	73	-27.3	29.21	73	-0.6
④ A-N-2-2	6-11-74	17:34	10	1942	29.09	72	-27.2	29.21	74	+0.2
A-N--B Blank for -N- Series										
7 - 26.0mls.										
8 - 24.5mls.										
9 - 24.0mls.										
10 - 25.5mls.										

STW INCORPORATED

NOx DATA SHEET

Customer: MARBLE HEAD LIME CO.

Installation: BUFFINGTON

Location: GARY, IND

Job No.: 73-109

Rate:

Test No.: 2

Amb. Temp:

Test Date: 6-12-74

Test By: D. J. W.

~~Stack~~ Stack #6, south port (Pilot tip was 34 inches in floor inside of stack)

Sample Bottle Number	Date	Time	Flask Number	Volume of Flask, ml	Initial Conditions			Final Conditions		
					Bar. Press. in. Hg	Flask Temp, of	Flask Vac. in. Hg	Bar. Press. in. Hg	Flask Temp, of	Flask Vac. in. Hg
5	6-12-74	12:23	1	1964	29.24	72	-27.2	29.18	80	+5
6	6-12-74	13:05	2	2046	29.21	75	-27.4	29.16	81	-1
7	6-12-74	13:40	4	2009	29.20	76	-27.4	29.18	81	0
8	6-12-74	14:14	5	2020	29.18	71	-27.4	29.18	82	-3

-N- -B Blank for -N- Series

Sample Bottle #

5-25 ml

6-25 ml

7-25 ml

8-24 ml

788 08:00 - 17:30 = 9:30

Others 10:00 - 17:30 = 7:30

14.4
12.9
1.5

STW INCORPORATED

NO. DATA SHEET

Test No.: 3

Customer: MARBLE HEAD LIME CO.

Amb. Temp: 73

Installation: BUFFINGTON

Test Date: 6-13-74

Location: GARY, IND.

Test By: D. J. Waden

Job No.: 73-109

Rate:

Stack #3, south port (Probe tip 34 inches in from inside of stack) (Reading taken at 10:30-11:00 6-14-74)

Initial Conditions			Final Conditions		
Bar. Press.	Flask Temp.	Flask Vac.	Bar. Press.	Flask Temp.	Flask Vac.
in. Hg	of	in. Hg	in. Hg	of	in. Hg
29.22	77	-27.6	29.37	85	+0.3
29.19	78	-27.6	29.37	85	+0.2
29.22	82	-27.6	29.37	86	+0.1
29.18	80	-27.5	29.37	83	0

Sample Number	Date	Time	Flask Number	Volume of Flask, ml
10	6-13-74	11:04	8	2030
11	"	10:36	10	1992
12	"	11:36	11	2040
13	"	12:36	12	1994

Blank for -N- Series

Sample Bottle #	Volume of absorbing solution, ml
9	26
10	26
11	25
12	26

Source of Air Contaminants exhaust from lime kiln by house

Type of Air Contaminants _____

Point of Discharge: Stack ☒ Other series of 6 stacks

Point of Observation: _____

Distance to Base of Point of Discharge, feet 200 ft 100 ft

Height of Point of Discharge Above Ground Level, feet 200 ft 20 ft

Background Description SK

Weather: Clear ☐ Overcast ☒ Partly Cloudy ☐ Other _____

Wind Direction _____ Wind Velocity, mi/hr 20

Plume Description:

Detached: Yes ☐ No ☐

Color: Black ☐ White ☐ Other not observable

Plume Dispersion Behavior: Looping ☐ Coning ☐ Fanning ☐
Lofting ☐ Fumigating ☐ See Comments ☒

Estimated Distance (feet) Plume Visible (Maximum) _____ (Minimum) _____

Comments no visible plume mostly

Signed

James Pullman

Title

Chemical Technician

②

RECORD OF
VISIBLE EMISSIONS

TIME OF OBSERVATION: FROM 138 A.M. TO 238 A.M. DATE 6/11/74

Stack No. 1

[illegible]

NOTE: Each small square represents an individual reading of intensity corresponding to that shown in the left-hand column over a time span of 1/4 minute. Insert an "S" in the top row of blank squares to indicate the exact minute of the start of observation. In the next square after the "S", insert the hour in which the measurement was made. Each page of this form can thus be used to record 1 hour of measurements.

Source of Air Contaminants exhaust from line kiln baghouse

Type of Air Contaminants _____

Point of Discharge: Stack ☒ Other series of six stacks

Point of Observation:

Distance to Base of Point of Discharge, feet ~~2000~~ 100 ft

Height of Point of Discharge Above Ground Level, feet ~~2000~~ 80 ft

Background Description SKs

Weather: Clear ☐ Overcast ☒ Partly Cloudy ☐ Other _____

Wind Direction SE Wind Velocity, mi/hr 20

Plume Description:

Detached: Yes ☐ No ☐

Color: Black ☐ White ☐ Other not visible

Plume Dispersion Behavior: Looping ☐ Coning ☐ Fanning ☐
Lofting ☐ Furnigating ☐ See Comments ☒

Estimated Distance (feet) Plume Visible (Maximum) _____ (Minimum) _____

Comments no visible plume mostly

Signed

Garry Pulliam

Title

Chemical Technician

3

Marblehead Line

Stack No. 2

exhaust of 'house of Lime Kiln

356

A.M. 4/56 A.M.
P.M. TO P.M.

DATE 6/11/79

[illegible]

NOTE: Each small square represents an individual reading of intensity corresponding to that shown in the left-hand column over a time span of 1/4 minute. Insert an "S" in the top row of blank squares to indicate the exact minute of the start of observation. In the next square after the "S", insert the hour in which the measurement was made. Each page of this form can thus be used to record 1 hour of measurements.

#55tk Puffing @ 15% Opening

Source of Air Contaminants exhaust from lime kiln basker

Type of Air Contaminants _____

Point of Discharge: Stack ☐ Other series of six stacks

Point of Observation:

Distance to Base of Point of Discharge, feet 300 ft 100 m

Height of Point of Discharge Above Ground Level, feet 200 ft 80 m

Background Description SK

Weather: Clear ☐ Overcast ☒ Partly Cloudy ☐ Other _____

Wind Direction SW Wind Velocity, mi/hr 20

Plume Description:

Detached: Yes ☐ No ☐

Color: Black ☐ White ☒ Other not observable mostly

Plume Dispersion Behavior: Looping ☐ Coning ☐ Fanning ☐
Lofting ☐ Fumigating ☐ See Comments ☒

Estimated Distance (feet) Plume Visible (Maximum) _____ (Minimum) _____

Comments No visible plume mostly

Signed _____ Title _____

4

Man-headed lion

EQUIPMENT LOCATION (ADDRESS)

extent of cashed time (hr)

TIME OF OBSERVATION: FROM

A.M. 5:50 A.M. ✓
P.M. TO P.M.

DATE 6-11-74

Stack No. 2

[illegible][illegible][illegible]

NOTE: Each small square represents an individual reading of intensity corresponding to that shown in the left-hand column over a time span of 1/2 minute. Insert an "S" in the top row of blank squares to indicate the exact minute of the start of observation. In the next square after the "S", insert the hour in which the measurement was made. Each page of this form can thus be used to record 1 hour of measurements.

Source of Air Contaminants

2 short plume like buildings

Type of Air Contaminants

Point of Discharge:

Stack

☐

Other

Series of six stacks

Point of Observation:

Distance to Base of Point of Discharge, feet

200 ft

Height of Point of Discharge Above Ground Level, feet

80 ft

Background Description

SKY

Weather:

Clear

☐

Overcast

☐

Partly Cloudy

☐

Other

Wind Direction

SW

Wind Velocity, mi/hr

20

Plume Description:

Detached:

Yes

☐

No

☐

Color:

Black

☐

White

☐

Other

not observable mostly

Plume Dispersion Behavior:

Looping

☐

Coning

☐

Fanning

☐

Lofting

☐

Fumigating

☐

See Comments

☐

Estimated Distance (feet) Plume Visible (Maximum)

(Minimum)

Comments

No visible emission

Signed

Title

ENVIRONMENTAL PROTECTION AGENCY

COMPANY NAME MARBLEHEAD LIME Co.

EQUIPMENT LOCATION (ADDRESS) GARY, IND.

TIME OF OBSERVATION: FROM 17:01 ^{A.M.} _{P.M.} TO 18:01 ^{A.M.} _{P.M.} DATE 6-11-74

RECORD OF VISIBLE EMISSIONS

STACKS 1+2

[illegible][illegible][illegible]

NOTE: Each small square represents an individual reading of intensity corresponding to that shown in the left-hand column over a time span of $\frac{1}{4}$ minute. Insert an "S" in the top row of blank squares to indicate the exact minute of the start of observation. In the next square after the "S", insert the hour in which the measurement was made. Each page of this form can thus be used to record 1 hour of measurements.

Source of Air Contaminants LIME KILN

Type of Air Contaminants PARTICULATE, SO₂, NO_x, CO

Point of Discharge: Stack ☒ Other #1 & #2

Point of Observation:

Distance to Base of Point of Discharge, feet ~100

Height of Point of Discharge Above Ground Level, feet 30

Background Description SKY

Weather: Clear ☐ Overcast ☐ Partly Cloudy ☒ Other _____

Wind Direction _____ Wind Velocity, mi/hr 5-10

Plume Description:

Detached: Yes ☐ No ☐

Color: Black ☐ White ☐ Other NONE

Plume Dispersion Behavior: Looping ☐ Coning ☐ Fanning ☐
Lofting ☐ Furnigating ☐ See Comments ☐

Estimated Distance (feet) Plume Visible (Maximum) _____ (Minimum) _____

Comments _____

Signed V. W. Brown Title _____

Source of Air Contaminants LIME KILN

Type of Air Contaminants PARTICULATE, SO₂, NO_x, CO

Point of Discharge: Stack ☒ Other #1 & #2

Point of Observation:

Distance to Base of Point of Discharge, feet ~ 100

Height of Point of Discharge Above Ground Level, feet 80

Background Description SKY

Weather: Clear ☐ Overcast ☒ Partly Cloudy ☐ Other _____

Wind Direction SW Wind Velocity, mi/hr 5-15

Plume Description:

Detached: Yes ☐ No ☐

Color: Black ☐ White ☐ Other NONE

Plume Dispersion Behavior: Looping ☐ Coning ☐ Fanning ☐
Lofting ☐ Furnigating ☐ See Comments ☐

Estimated Distance (feet) Plume Visible (Maximum) _____ (Minimum) _____

Comments LIGHT INTERMITTENT SHOWERS

Signed J. W. Brown Title _____

Source of Air Contaminants Lime Kiln

Type of Air Contaminants Particulate SO₂, NO_x, CO

Point of Discharge: Stack ☒ Other 3 + 4

Point of Observation:

Distance to Base of Point of Discharge, feet 100' Observed from #4 Scaffold

Height of Point of Discharge Above Ground Level, feet 80'

Background Description sky

Weather: Clear ☒ Overcast ☐ Partly Cloudy ☐ Other _____

Wind Direction _____ Wind Velocity, mi/hr _____

Plume Description:

Detached: Yes ☐ No ☐

Color: Black ☐ White ☒ Other Not Visible Mostly

Plume Dispersion Behavior: Looping ☐ Coning ☐ Fanning ☐
Lofting ☐ Fumigating ☐ See Comments ☐

Estimated Distance (feet) Plume Visible (Maximum) _____ (Minimum) _____

Comments _____

Signed James Pulliam Title Chemical Technician

20

RECORD OF
VISIBLE EMISSIONS

exhaust of benz house of lime Kda

Stack No. 3

[illegible]

NOTE: Each small square represents an individual reading of intensity corresponding to that shown in the left-hand column over a time span of 1/4 minute. Insert an "S" in the top row of blank squares to indicate the exact minute of the start of observation. In the next square after the "S", insert the hour in which the measurement was made. Each page of this form can thus be used to record 1 hour of measurements.

Source of Air Contaminants exhaust stack brickhouse line kiln

Type of Air Contaminants Particulate Non SO₂

Point of Discharge: Stack ☒ Other 11

Point of Observation:

Distance to Base of Point of Discharge, feet 100' Observed from #4 Scaffold

Height of Point of Discharge Above Ground Level, feet 80'

Background Description _____

Weather: Clear ☒ Overcast ☐ Partly Cloudy ☐ Other _____

Wind Direction SW Wind Velocity, mi/hr 20

Plume Description:

Detached: Yes ☐ No ☐

Color: Black ☐ White ☒ Other Not Visible Mostly

Plume Dispersion Behavior: Looping ☐ Coning ☐ Fanning ☐
Lofting ☐ Furnigating ☐ See Comments ☐

Estimated Distance (feet) Plume Visible (Maximum) _____ (Minimum) _____

Comments _____

Signed Harry Pulliam Title Chem Tech

3

Test #2

Marblehead Line

exhibit of bank house of line Kien

142

A.M. 242 A.M.
P.M. TO 2 P.M.

DATE 6/12/74

Stack No. 4

[illegible]

NOTE: Each small square represents an individual reading of intensity corresponding to that shown in the left-hand column over a time span of 1/4 minute. Insert an "S" in the top row of blank squares to indicate the exact minute of the start of observation. In the next square after the "S", insert the hour in which the measurement was made. Each page of this form can thus be used to record 1 hour of measurements.

Source of Air Contaminants Line Kilo Base Stk.

Type of Air Contaminants Particulate. Nox SO.

Point of Discharge: Stack ☒ Other _____

Point of Observation:

Distance to Base of Point of Discharge, feet 100'

Height of Point of Discharge Above Ground Level, feet 80'

Background Description SKY

Weather: Clear ☐ Overcast ☐ Partly Cloudy ☒ Other _____

Wind Direction SW Wind Velocity, mi/hr 20

Plume Description:

Detached: Yes ☐ No ☐

Color: Black ☐ White ☒ Other Not Visible Mostly

Plume Dispersion Behavior: Looping ☐ Coning ☐ Fanning ☐
Lofting ☐ Fumigating ☐ See Comments ☐

Estimated Distance (feet) Plume Visible (Maximum) _____ (Minimum) _____

Comments _____

Signed Ray Pulliam Title Chem. Tech.

Source of Air Contaminants Line Kiln Baghouse Stk

Type of Air Contaminants Particulate NOx SO₂

Point of Discharge: Stack ☒ Other _____

Point of Observation:

Distance to Base of Point of Discharge, feet 100'

Height of Point of Discharge Above Ground Level, feet 80'

Background Description _____

Weather: Clear ☐ Overcast ☐ Partly Cloudy ☒ Other _____

Wind Direction _____ Wind Velocity, mi/hr _____

Plume Description:

Detached: Yes ☐ No ☐

Color: Black ☐ White ☒ Other Not Visible Mostly

Plume Dispersion Behavior: Looping ☐ Coning ☐ Fanning ☐
Lofting ☐ Furnigating ☐ See Comments ☐

Estimated Distance (feet) Plume Visible (Maximum) _____ (Minimum) _____

Comments _____

Signed

Gary Pulliam

Title

Chem Tech.

COMPANY NAME MARBLEHEAD Line Co.

EQUIPMENT LOCATION (ADDRESS) BAEHOUSE STAIRS No. 5 (STACK #3)

RECORD OF VISIBLE EMISSIONS

EQUIPMENT LOCATION (ADDRESS) _____
TIME OF OBSERVATION: FROM 10:53 A.M. TO _____ P.M. DATE 6/12/74

[illegible][illegible][illegible]

NOTE: Each small square represents an individual reading of intensity corresponding to that shown in the left-hand column over a time span of 1/4 minute. Insert an "S" in the top row of blank squares to indicate the exact minute of the start of observation. In the next square after the "S", insert the hour in which the measurement was made. Each page of this form can thus be used to record 1 hour of measurements.

Source of Air Contaminants _____

Type of Air Contaminants _____

Point of Discharge: Stack ☐ Other _____

Point of Observation:

Distance to Base of Point of Discharge, feet _____

Height of Point of Discharge Above Ground Level, feet _____

Background Description _____

Weather: Clear ☐ Overcast ☐ Partly Cloudy ☐ Other _____

Wind Direction _____ Wind Velocity, mi/hr. _____

Plume Description:

Detached: Yes ☐ No ☐

Color: Black ☐ White ☐ Other _____

Plume Dispersion Behavior: Looping ☐ Coning ☐ Fanning ☐
Lofting ☐ Fumigating ☐ See Comments ☐

Estimated Distance (feet) Plume Visible (Maximum) _____ (Minimum) _____

Comments _____

Signed _____ Title _____

ENVIRONMENTAL PROTECTION AGENCY

COMPANY NAME MARBLEHEAD LIME CO.

RECORD OF
VISIBLE EMISSIONS

EQUIPMENT LOCATION (ADDRESS) CARY, INDIANA

TIME OF OBSERVATION: FROM 11:53 ^{A.M.} TO 12:53 ^{A.M.} DATE 6-17-74

STACK #3

Start/hour																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																					</
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Start/hour																						
R. No.	%	Min.	41	42	43	44	45	46	47	48	49	50	51	52	53	54	55	56	57	58	59	60
5	100																					
4 1/2	95																					
4 1/4	90																					
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4	80																					
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3 1/8	65																					
3	60																					
2 1/2	55																					
2 1/4	50																					
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2	40																					
1 1/2	35																					
1 1/4	30																					
1 1/8	25																					
1	20																					
1/2	15																					
1/4	10																					
1/8	5																					
0	0																					

NOTE: Each small square represents an individual reading of intensity corresponding to that shown in the left-hand column over a time span of 1/4 minute. Insert an "S" in the top row of blank squares to indicate the exact minute of the start of observation. In the next square after the "S", insert the hour in which the measurement was made. Each page of this form can thus be used to record 1 hour of measurements.

Source of Air Contaminants #5 LIME KILN BAGHOUSE

Type of Air Contaminants PARTICULATE, SO₂, NO_x, CO

Point of Discharge: Stack ☒ Other STACK #3

Point of Observation:

Distance to Base of Point of Discharge, feet ~90 OBSERVED FROM #4 SCAFFOLD

Height of Point of Discharge Above Ground Level, feet 30

Background Description _____

Weather: Clear ☐ Overcast ☐ Partly Cloudy ☒ Other _____

Wind Direction SW Wind Velocity, mi/hr ~20 GUSTS TO 35

Plume Description:

Detached: Yes ☐ No ☐

Color: Black ☐ White ☐ Other NONE VISIBLE

Plume Dispersion Behavior: Looping ☐ Coning ☐ Fanning ☐
Lofting ☐ Furnigating ☐ See Comments ☐

Estimated Distance (feet) Plume Visible (Maximum) _____ (Minimum) _____

Comments _____

Signed J. W. Brown Title _____

ENVIRONMENTAL PROTECTION AGENCY

COMPANY NAME MOBILEBAND LIME CO.

EQUIPMENT LOCATION (ADDRESS) 6.824, 1.051A0A

TIME OF OBSERVATION: FROM 13:05 P.M. TO 14:05 P.M. DATE 6-12-74

RECORD OF VISIBLE EMISSIONS

STACK #4

[illegible][illegible][illegible]

NOTE: Each small square represents an individual reading of intensity corresponding to that shown in the left-hand column over a time span of 1/4 minute. Insert an "S" in the top row of blank squares to indicate the exact minute of the start of observation. In the next square after the "S", insert the hour in which the measurement was made. Each page of this form can thus be used to record 1 hour of measurements.

Source of Air Contaminants #5 LIME KILN BAGHOUSE

Type of Air Contaminants PARTICULATE, SO₂, NO_x, CO

Point of Discharge: Stack ☒ Other STACK # 4

Point of Observation:

Distance to Base of Point of Discharge, feet ~ 200

Height of Point of Discharge Above Ground Level, feet 80

Background Description SKY

Weather: Clear ☐ Overcast ☐ Partly Cloudy ☒ Other _____

Wind Direction SW Wind Velocity, mi/hr 15

Plume Description:

Detached: Yes ☐ No ☐

Color: Black ☐ White ☐ Other NONE VISIBLE

Plume Dispersion Behavior: Looping ☐ Coning ☐ Fanning ☐
Lofting ☐ Fumigating ☐ See Comments ☐

Estimated Distance (feet) Plume Visible (Maximum) _____ (Minimum) _____

Comments _____

Signed J.W. Brown Title _____

ENVIRONMENTAL PROTECTION AGENCY

COMPANY NAME HARBLEHEAD LIME CO.

EQUIPMENT LOCATION (ADDRESS) GARY, INDIANA

TIME OF OBSERVATION: FROM 11:05 A.M. TO 11:05 A.M. DATE 6-12-77

RECORD OF
VISIBLE EMISSIONS

STACK # 4

Start/ hour																						
R. No.	%	Min.	01	02	03	04	05	06	07	08	09	10	11	12	13	14	15	16	17	18	19	20
5	100																					
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NOTE: Each small square represents an individual reading of intensity corresponding to that shown in the left-hand column over a time span of 1/2 minute. Insert an "S" in the top row of blank squares to indicate the exact minute of the start of observation. In the next square after the "S", insert the hour in which the measurement was made. Each page of this form can thus be used to record 1 hour of measurements.

Source of Air Contaminants #5 LIME KILN BAGHOUSE

Type of Air Contaminants PARTICULATE, SO₂, NO_x, CO

Point of Discharge: Stack ☒ Other STACK #4

Point of Observation:

Distance to Base of Point of Discharge, feet ~ 200

Height of Point of Discharge Above Ground Level, feet 80

Background Description SKY

Weather: Clear ☐ Overcast ☐ Partly Cloudy ☒ Other _____

Wind Direction _____ Wind Velocity, mi/hr ~ 10

Plume Description:

Detached: Yes ☐ No ☐

Color: Black ☐ White ☐ Other NONE VISIBLE

Plume Dispersion Behavior: Looping ☐ Coning ☐ Fanning ☐
Lofting ☐ Furnigating ☐ See Comments ☐

Estimated Distance (feet) Plume Visible (Maximum) _____ (Minimum) _____

Comments _____

Signed

J.W. Brown

Title _____

NOTE: Each small square represents an individual reading of intensity corresponding to that shown in the left-hand column over a time span of 1/4 minute. Insert an "S" in the top row of blank squares to indicate the exact minute of the start of observation. In the next square after the "S", insert the hour in which the measurement was made. Each page of this form can thus be used to record 1 hour of measurements.

Line Kiln Bayhouse

Particulate, SO_2 , NO_x , CO

Stack # 5

Observed from # 4 scaffold - stack base 80', height 100'

Background - sky

Weather - Partly cloudy

Wind ~ 20 MPH from S

No visible plume

By Gary Pothorn - Walden

ENVIRONMENTAL PROTECTION AGENCY

COMPANY NAME

EQUIPMENT LOCATION (ADDRESS)

TIME OF OBSERVATION: FROM 10.30

RECORD OF VISIBLE EMISSIONS

STACK #5

[illegible][illegible][illegible]

NOTE: Each small square represents an individual reading of intensity corresponding to that shown in the left-hand column over a time span of 1/4 minute. Insert an "S" in the top row of blank squares to indicate the exact minute of the start of observation. In the next square after the "S", insert the hour in which the measurement was made. Each page of this form can thus be used to record 1 hour of measurements.

ENVIRONMENTAL PROTECTION AGENCY

COMPANY NAME

EQUIPMENT LOCATION (ADDRESS)

TIME OF OBSERVATION:

RECORD OF

VISIBLE EMISSIONS

STACK #6

[illegible][illegible][illegible]

NOTE: Each small square represents an individual reading of intensity corresponding to that shown in the left-hand column over a time span of 1/4 minute. Insert an "S" in the top row of blank squares to indicate the exact minute of the start of observation. In the next square after the "S", insert the hour in which the measurement was made. Each page of this form can thus be used to record 1 hour of measurements.

Lime Kiln Baghouse.

formaldehyde, SO₂, NO_x, CO

Stack # 6

Observed from ground - ~200' from base. Stack - 80' high

Background - clear

Weather - overcast

Wind: 5-10 MPH from S-SW

No visible plume

By Gary Pulliam - Weldon

ENVIRONMENTAL PROTECTION AGENCY

COMPANY NAME MARLBORO Line Co.

EQUIPMENT LOCATION (ADDRESS) GARY, INDIANA

TIME OF OBSERVATION: FROM 12:46 ^{A.M.} _{P.M.} TO 13:46 ^{A.M.} _{P.M.} DATE 6-13-74

RECORD OF VISIBLE EMISSIONS

STACK #6

[illegible][illegible][illegible]

NOTE: Each small square represents an individual reading of intensity corresponding to that shown in the left-hand column over a time span of 1/2 minute. Insert an "S" in the top row of blank squares to indicate the exact minute of the start of observation. In the next square after the "S", insert the hour in which the measurement was made. Each page of this form can thus be used to record 1 hour of measurements.

Yine Kiler Baghouse

Particulate, SO₂, NO_x, CO

Stack # 6

Observed from ground - ~200' from base. Stack - 90' high.

Background - clear

Weather - overcast

Wind: 5-10 MPH from S-SW

No visible plume

By Doug Pulliam-Walton

Location: Lime Kiln #5

Stack: #6

Background: Overcast Sky

Height of stack - 80'

Height of observation - ground

Distance from observer to stack ~ 200'

Wind Speed: 5-10 mph

" Direction: S-SW

No visible plume

John W. Brown

Location: Lime Kiln #5 Baghouse

Stack: #6

Background: Overcast Sky

Height of Stack: 80'

Point of observation: ground

Distance from stack: ~200'

Wind Speed: 5-10 mph

1. Direction: S-SW

No visible ^{plume} ~~plume~~

John W. Brown

APPENDIX G
STANDARD SAMPLING PROCEDURES

A. PARTICULATE SAMPLING (EPA METHOD 5)

The selection of sampling sites and the number of traverse points for particulate sampling was performed in accordance with EPA Method 1, Federal Register, December 23, 1971. There are two 3" sampling ports on each of the six stacks. They are located 90° apart, 2' from the outlet and 6' from the inlet. The stacks are 7'4" in diameter and therefore required the maximum number of traverse points (48). Samples were taken at each of the 48 points for five minutes per point or a total of 240 minutes (four hours) for each run.

Preliminary pitot traverses were performed on June 10, 1974, in accordance with Method 2, Federal Register, December 23, 1971, to determine the stack gas velocity. Measurements of the velocity head using a Type S (Stauscheibe) pitot tube and inclined manometer and stack temperature using a thermocouple were recorded and are presented in Appendix F. The stack gas molecular weight was determined by three 4-hour integrated Orsat gas analyses simultaneously with the particulate tests as indicated in Method 3, Federal Register, December 23, 1971. The stack gas velocity and the volumetric flow rates were calculated for each test in Walden's computer program and presented in the summary results. The equations used to calculate the stack gas velocity and the volumetric flow rate were Equations 2-2 and 2-3, respectively, of the Federal Register, December 23, 1971.

Percent moisture in the gas stream was determined by a wet bulb - dry bulb technique. A 3/4-inch standard pipe fitted with a standard "tee" and a connection to a pump was inserted into the test port. A dry bulb thermometer with rubber stopper and a wet bulb thermometer were placed in the tee. The proper temperatures were obtained by regulating the rate of flow at 1.5 cubic feet per minute to obtain a flow of at least six hundred feet per minute in accordance with tables computed from U.S. Bureau of Standards data.

The particulate sampling train was a Joy Manufacturing Emission Parameter Analyzer with a 13-foot stainless steel probe. A six-foot glass-lined probe was not long enough to completely traverse the duct diameter,



therefore, the EPA Project Officer granted approval for the use of a stainless steel probe. The control unit contained the temperature and pressure instrumentation, vacuum source, temperature-compensated dry gas meter, and interval timer. It should be noted that the computer data sheets indicate the meter temperature to be 70°F due to temperature compensation within the control unit. The design specifications of this particulate sampling train comply with standards set forth in APTD-0581. EPA approval was also granted for the use of stationary impingers connected to the traversing probe and heater box through flexible Teflon tubing. The sampling train is shown in Figure G-1.

The variations from Method 5 as described in the Federal Register were the addition of one hundred milliliters of water to the third impinger and the use of a stationary impinger box connected to the heated filter box through Teflon tubing. Normally, the third impinger is left empty, however, the addition of water did not alter the sampling methods or results as the water was eventually evaporated in a beaker for the determination of particulate matter in the residual water fraction.

Due to the low velocities (about 15 feet per second), inclined manometers with a range of 0 - 0.25 inches H₂O were used. Nomographs were not used for the adjustment of the sampling rate, rather the equations that serve as the basis for the nomograph were calculated. A direct relationship between the stack velocity head (ΔP_s) and the pressure differential across the orifice meter (ΔH) was determined and used for setting the isokinetic sampling rate. The relationship is as follows:

$$\left[\frac{(2.9) (P.C.F.) (60) (\pi) (D)^2 (1-B) (T_m)}{4(144) (T_s)^{1/2} (O.C.F.)} \right]^2 \Delta P = \Delta H$$

where:

- STD P.C.F. = Pitot correction factor (dimensionless)
- D = Diameter of nozzle, inches
- B = Percent moisture in gas stream
- T_m = Meter temperature, °R
- T_s = Stack temperature, °R
- O.C.F. = Orifice correction factor

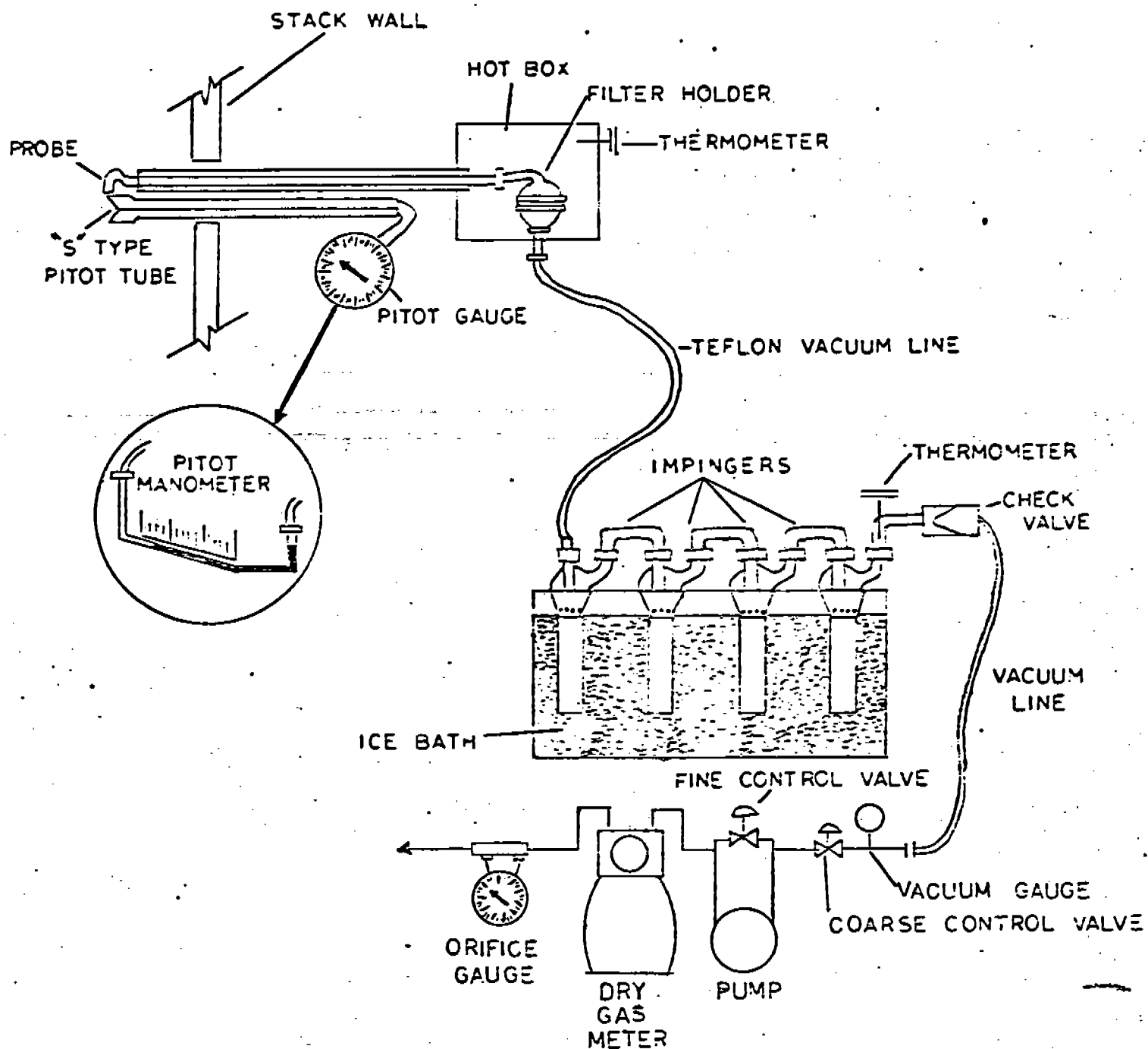


Figure G-1. Particulate Sampling Train,
Marblehead Lime, Gary, Indiana

Also, a meter rate formula was determined and used to maintain isokinetic flow by checking the flow rate at 15-second intervals. We have found this approach to be quite accurate as the two equations serve as a check for each other. The meter rate formula is as follows:

$$M_r = (P.C.F.) \times V_{avg.} \times 60 \times \frac{T_m}{T_s} \times \frac{P_b \pm P_s}{P_b - P_m} \times A_n \times (1 - \%H_2O).$$

where:

M_r = Volumetric flow rate, $ft^3/min.$

P.C.F. = Pitot correction factor (dimensionless)

$V_{avg.}$ = Average velocity, ft/sec

T_m = Meter temperature, $^{\circ}R$

T_s = Stack temperature, $^{\circ}R$

P_b = Barometric pressure, in. Hg.

P_s = Stack static pressure, in. Hg.

P_m = Vacuum at meter, in. Hg.

A_n = Area of nozzle, ft^2

$\%H_2O$ = Percent moisture in gas stream

The stack gas molecular weight was determined by three 4-hour integrated gas analyses collected simultaneously with the particulate tests. An Orsat was used to determine CO_2 and Fyrites were used to determine CO_2 and O_2 . The Orsat scale is only capable of reading up to 21%. Since the O_2 is read together with the CO_2 , a reading above 21% (16.5% O_2 and 7.0% CO_2 = 23.5% total) was obtained and therefore, Fyrites were used.

Three and one-half-inch diameter glass fiber filters were desiccated for 48 hours and weighed to the nearest 0.5 milligram on a Satorius Model 2742 analytical balance prior to the test period. Also, approximately two hundred grams of silica gel were weighed to the nearest gram and placed in storage bottles for use in the field. The sampling train was prepared by placing a preweighed glass fiber filter into a pyrex glass filter holder with a heating system capable of maintaining a minimum temperature of $225^{\circ}F$. One hundred milliliters of distillate water was placed in each of the first three impingers and preweighed silica gel was placed in

the fourth impinger. The impingers were connected in series with glass ball joint fittings. The first, third and fourth impingers were of the Greenburg-Smith design, modified by replacing the tip with a one-half-inch ID glass tube extending to one-half inch from the bottom of the flask. The second impinger was of the Greenburg-Smith design with the standard tip. The addition of one hundred milliliters of water to the third impinger was an error in the field preparation.

Sample recovery and analysis were performed in accordance with the methods described in the Federal Register, August 17, 1971. At the request of the Project Officer, a front-half water wash was performed after the acetone wash. This procedure should be used when testing lime kilns due to the nature of the particulate emissions. All sample bottles were acid-washed in accordance with specifications requested by the EPA. The Wheaton bottles in accordance with specifications requested by the EPA. The tared beakers and filters containing the particulate matter will be held by EPA for their use.

Following completion of each repetition, the sample recovery procedure was conducted in the laboratory within the plant facility. Portions of the distilled water and acetone used were set aside as blanks for analysis. The filter was removed from its holder and placed in a container along with any filter residue clinging to the filter holder. All loose particulate matter from all sample-exposed surfaces prior to the filter was washed with acetone and placed in a second labeled container. The volume of water from the first three impingers was measured and placed in a third container along with water rinsings of all sample-exposed surfaces between the filter and fourth impinger. This included the flexible Teflon tubing. The silica gel was weighed and placed in a fourth container. Finally, all sample-exposed surfaces between the filter and fourth impinger were rinsed with acetone and placed in a fifth container.

All samples were returned to the Walden laboratories and analyzed. The filter and loose particulate matter was dried, dessicated, and weighed over a 72-hour period. The front-half acetone washings were evaporated to dryness under a hood in a tared beaker at ambient temperature and pressure. The beaker was then dried, dessicated and weighed. Three 25 milliliter

portions of chloroform were individually added to a separatory funnel containing the water washings from the impinger catch. The extraction was completed with three 25 milliliter portions of ethyl ether and both the ether and chloroform extracts combined in a tared beaker. The extracts were evaporated at 70°F under a hood and then dried, dessicated, and weighed. The back half acetone washings were treated in a similar manner as the front-half acetone washings.

B. SULFUR DIOXIDE SAMPLING (EPA METHOD 6)

Six sulfur dioxide tests were run at the outlet in accordance with Test Method 6 as described in the Federal Register, December 23, 1971. The sampling period was to be four hours, however, carry-over from the first impinger containing isopropanol occurred prior to the end of the test. To avoid carrying over the sulfuric acid fraction into the sulfur dioxide fraction, the tests were terminated at this point. The sampling system consisted of a Walden-built control module containing the temperature and pressure instrumentation, vacuum source, dry gas meter, rotameter, and drying tube, three midget impingers, one midget bubbler, a three-foot heated glass-lined probe, and a pitot tube. The sampling point was chosen, as the average velocity point and proportional gas sampling was easily maintained as only minor variations were noted in the stack gas velocity during these runs. Leak checks were run prior to each repetition by plugging the probe inlet and pulling 10 inches Hg. vacuum. A leakage rate less than one percent of the sampling rate was found for each run.

The sampling reagents were prepared prior to the tests and added to the sampling trains at the test site. Eighty percent isopropanol was made up by mixing 160 milliliters of isopropanol to forty milliliters of deionized, distilled water. Three percent hydrogen peroxide was made up by diluting two hundred milliliters of thirty percent hydrogen peroxide to two liters with deionized distilled water. The hydrogen peroxide was prepared fresh daily.

Fifteen milliliters of eighty percent isopropanol was poured into a midget bubbler and fifteen milliliters of three percent hydrogen peroxide was poured into each of the first two midget impingers. The final midget impinger was left empty. The sampling system was set up as shown in Figure G-2. Quartz wool was packed into the probe end and crushed ice placed around the impingers.

Sample collection was performed by adjusting the sample flow rate proportional to the stack gas velocity. Since the sample is taken at a single point, variations in velocity were minimal and the sample flow rate was maintained at the original setting of one liter per minute. Readings were taken every five minutes during the tests. Upon completion of each sample run, the train was purged for 15 minutes with charcoal filtered ambient air. The contents in the midget bubbler were discarded and the contents in the midget impingers were stored in glass Wheaton bottles along with the distilled water washings.

The sulfur dioxide samples were returned to the Walden labs for analysis. The concentration of SO_2 in the samples was determined by the Barium-Thorin titration method described in the Federal Register. The procedure calls for the samples to be diluted to fifty milliliters with deionized water. Since some sample volumes exceeded fifty milliliters, all samples were diluted to 100 milliliters and twenty milliliter aliquots were obtained and diluted with eighty milliliters of certified reagent grade 2-propanol. Four drops of thorin indicator were added and titrated with a standardized barium perchlorate solution (0.0103N) to a pink end point. Two titrations were performed per sample and an average value determined.

The reagents used in the SO_2 analysis are as follows:

- (1) Barium perchlorate solution (0.0100N). Dissolve 1.9500 g barium perchlorate [$\text{Ba}(\text{ClO}_4)_2 \cdot 3 \text{H}_2\text{O}$] in 200 milliliter deionized water and dilute to one liter with reagent grade 2-propanol.

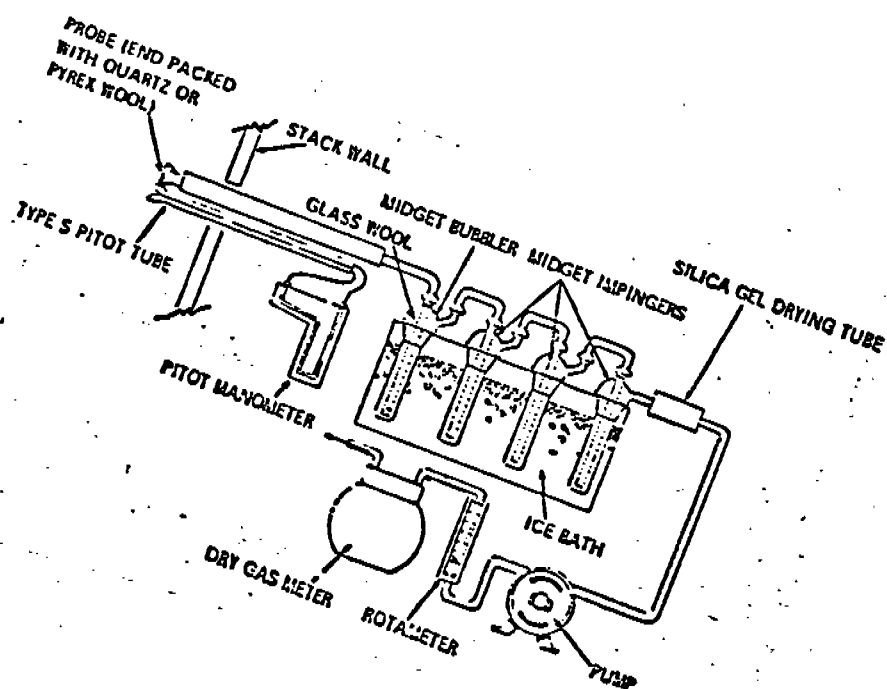


Figure G-2. SO_2 Sampling Train

- (2) Thorin indicator 1-(p-arsonophenyazo)2-naphthol-3,6-disulfonic acid. Dissolve 0.20 g disodium salt in one hundred milliliter distilled water.

C. NITROGEN OXIDES SAMPLING (EPA METHOD 7)

Twelve nitrogen oxides samples were collected at the outlet in accordance with the Federal Register, December 23, 1971, Method 7, and a modified draft procedure provided by the EPA. Four samples were obtained on June 10, 11, and 12 during the four hour particulate tests.

The sample collection flasks were two liter, Pyrex round bottom flasks with short neck and 24/40 standard taper opening encased in a protective foam covering. The absorbing solution was made up by adding 2.8 milliliters of concentrated sulfuric acid to one liter of distilled water with a graduated pipette. Twenty-five milliliters of absorbing solution was added to each flask prior to sampling and then the flask valve stopper inserted with the valve in the "purge" position. The sampling system was assembled as shown in Figure G-3 and the heated probe was located at the average velocity point for that port being sampled. All ground glass joints were greased with a high vacuum, high temperature chlorofluorocarbon based stopcock grease. The flask valve and pump valve were then turned to their "evacuate" positions and evacuated with the pump on. Upon evacuating the flask to three inches Hg absolute pressure, the pump valve was turned to the vent position and turned off. A leak check was made for the next minute by checking for fluctuations in the mercury level in the manometer. The flask volume, temperature, and barometric pressure were recorded and the flask valve and pump valve turned to their "purge" positions. The probe and tubing were purged with a squeeze bulb. The pump was then turned to its "vent" position and the flask valve to its "evacuate" position and the difference in mercury levels in the manometer recorded. The flask valve was immediately turned to its "sample" position and the gas was allowed to enter the flask until pressures in the flask and sample lines were equal. Finally, the flask valve was turned to its "purge" position and the flask shaken for five minutes.

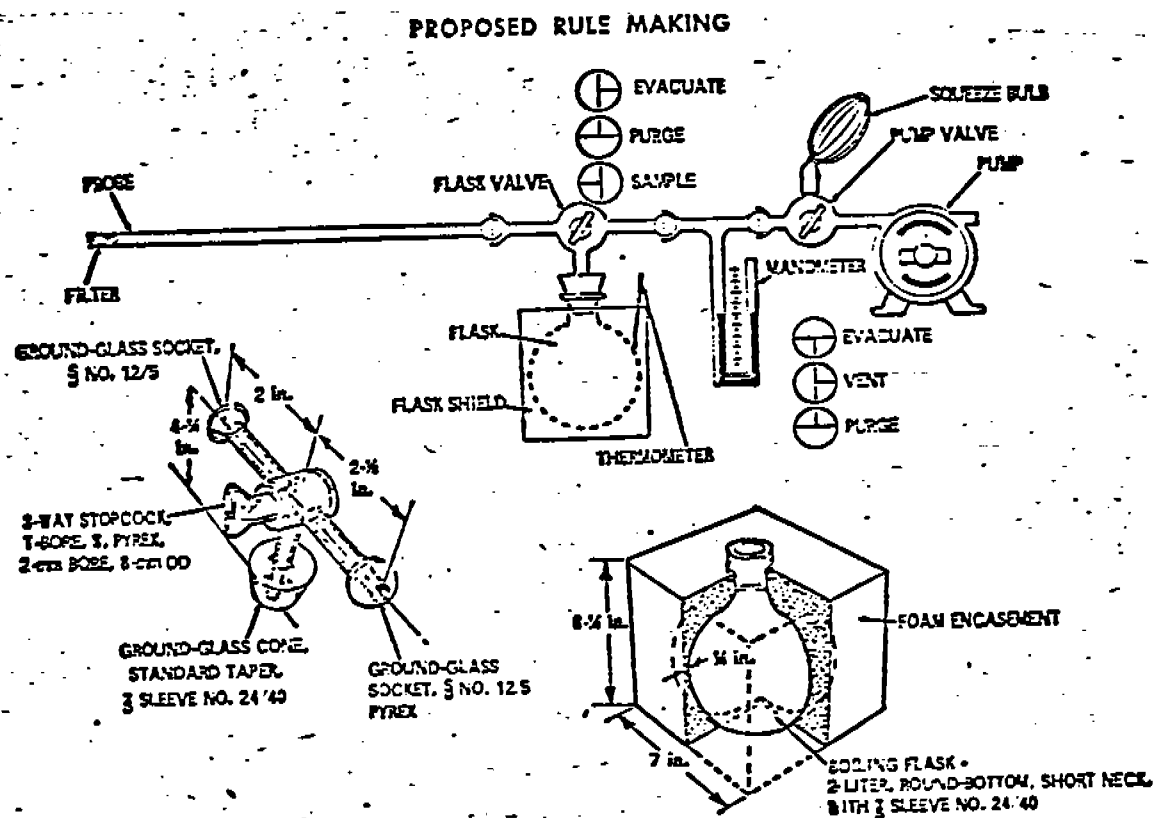


Figure G-3. Nitrogen Oxides Sampling System

The following day (approximately 24 hours) the contents of the flasks were shaken for two minutes. The flask was then connected to a mercury filled U-tube manometer, opening the valve from the flask and recording the flask temperature, pressure and the barometric pressure. The flask contents were transferred to glass Wheaton bottles for shipment to the laboratory. The flasks were rinsed with two five milliliter portions of deionized distilled water and the rinse water added to the storage bottles.

The concentration of NO_x samples were measured colorimetrically on a Beckman Spectronic 20, using the phenoldisulfonic acid (PDS) procedure. The procedure calls for a blank and a set of standards to be processed with the samples. The results of the colorimetric analysis are then used to calculate the sample concentrations.

After shipping, sodium hydroxide was added to the contents of the samples and the blank until the pH was 9-12. Each sample was quantitatively transferred to a two hundred and fifty milliliter evaporating dish, evaporated to dryness on a steam bath, and cooled. Next, two milliliters of phenoldisulfonic acid were added such that it made contact with all of the residue. One milliliter of deionized water was added and the samples were heated on the steam bath for three minutes, with stirring and cooling. Twenty milliliters of distilled water were added to the samples and concentrated ammonium hydroxide was added dropwise until a pH of 10 was reached, as determined by pH paper. Each sample was then transferred quantitatively to a one hundred milliliter volumetric flask and diluted to the mark with deionized water. A set of standards and the blank was prepared by pipeting 0.0, 1.0, 2.0, 3.0 and 4.0 milliliters of the potassium nitrate working solution into a two hundred and fifty milliliter evaporating dish. To each sample, ten milliliters of deionized water was added and then sodium hydroxide (1N) was added dropwise until a pH of 9-12 was reached. They were then diluted volumetrically to 100 milliliters and analyzed spectrophotometrically at 410 nm using the blank as the zero reference.

The reagents used in the analysis are as follows:

- (1) Phenoldisulfonic acid. Dissolve 25 g of pure white phenol in 150 milliliters concentrated sulfuric acid on a steam bath. Cool, add 75 milliliters fuming sulfuric acid and heat at 100°C for two hours. Store in dark stoppered bottle.
- (2) Potassium nitrate standard solution. Stock soln. Dissolve exactly 2.1980 g dry potassium nitrate (KNO_3) in deionized water and dilute to one liter. Working solution. Dilute 10 milliliters of stock solution to 100 milliliters with deionized water. One milliliter of working solution is equivalent to 100 μg NO_2 .
- (3) Absorbing reagent. Add 2.8 milliliters concentrated H_2SO_4 to one liter deionized water. Mix well and add 6 milliliters of 3% hydrogen peroxide.
- (4) Sodium hydroxide (1N). Dissolve 40 g NaOH in deionized water and dilute to one liter.

D. CARBON MONOXIDE SAMPLING (METHOD 10)

CO was measured according to EPA Method 10 by Honeywell Corporate Research using a Honeywell NDIR CO Analyzer. The bag samples represented approximately 2-hour accumulations and were run on three consecutive days.

The instrumentation for the measurements at Marblehead Lime Company was housed in a mobile van. The bag samples were collected through a probe and condenser sampling from a port near the top of the stack (about 80' high). A three-channel Honeywell NDIR Analyzer was used in this study. Although CO, CO_2 and CH_4 channels were available, only the CO channel was monitored.

After analysis of the bag sample on the Honeywell NDIR Analyzer, the CO concentration in the stack was determined from Equation 10-1 of the Federal Register, Volume 39, No. 47, March 8, 1974, page 9320.

EPA Method 10 specifies that for both integrated (bag) and continuous sampling, the sample must pass through a volume of silica gel and another of ascarite immersed in an ice bath (to remove H_2O and CO_2). Tests with the Honeywell NDIR CO Analyzer have demonstrated rejection ratios greater than 10^4 for both H_2O and CO_2 . Therefore, passing the sample through silica gel

and ascarite is unnecessary. In fact, passing the sample through the ascarite caused considerable technical difficulty. After about an hour of sampling, the ascarite formed a hard ball around the inlet tube to the ascarite container, causing a severe flow restriction.

E. OPACITY READINGS (METHOD 9)

The relative opacity of each of the six stacks was determined in accordance with Method 9 of the Federal Register, December 23, 1971. The opacity determinations were conducted for two hours on each stack during the particulate tests. Two observers read each stack except Stack No. 5, which was read by one observer.

APPENDIX H
LABORATORY REPORT

SAMPLE IDENTIFICATION LOG 6-11-74
Marblehead Lime Co. Gary, Indiana

EPA Number	Sample Location	Run	Contents	Comments
574-000-701	Stack #1	1-1	Filter	
" 702		"	Front half water wash	
" 703		"	" " acetone wash	
" 704		"	Back half water wash	VOID Washed by sampler, no residue left.
" 705		"	Back half water wash	
" 706		"	" " acetone wash	
" 707		"	Distilled water blank	
" 708		"	Acetone blank	
" 709	Stack #2	1-2	Filter	
" 710		"	Front half water wash	
" 711		"	" " acetone wash	
" 712		"	Back half water wash	VOID Washed by sampler, no residue left.
" 713		"	Back half water wash	
" 714		"	" " acetone wash	
" 715	Stack #5	1	Method 7 NOx	
" 716		2	"	
" 717		3	"	
" 718		4	"	
" 719	Stack #6	1	Method 6 SO ₂	
" 720		2	"	
" 721		1	Fuel	Limestone
" 722		1	Fuel	Pulverized Coal
" 723		1	Product	Lime
" 724		1	Dust	Baghouse collection
" 725	Stack #1	1-1	Silica gel	
" 726	Stack #2	1-2	Silica gel	
" 727	Stack #1	1-1	Silica-chloroform extract	
" 728	Stack #2	1-2	"	
" 729	Stack #3	2-3	"	
" 730	Stack #4	2-4	"	
" 731	Stack #5	3-5	"	
" 732	Stack #1	3-6	"	

* First number - run, Second number - stack

SAMPLE IDENTIFICATION LOG 6-12-74
Mottishine Time Co. Jang, Indiana

[illegible]

* First number - men, Second number - women

SAMPLE IDENTIFICATION LOG 6-13-74
Marblehead Lime Co. Bay, Indiana

[illegible]

1st First number - run, Second number - stock

MARBLEHEAD Lime CO.

G-337-9

FILTER	TARE	FINAL	STACK	SAMPLE #	DATE
#	<u>mg</u>	<u>mg</u>			
1	484.1	562.6	1	S-74-000-701	6/11
2	484.6	577.1	2	" 709	6/11
3	484.5	520.4	3	" 737	6/12
4	482.9	515.3	4	" 744	6/12
5	482.1	551.5	5	" 761	6/13
6	483.0	530.0	6	" 766	6/13

250 ML. BEAKERS

EXP NO.	CONTRACT NO.	TYPE	BEAKER NO.	FINAL	TARE WT.	GAIN
S-74-000-703	C-337-9	F.H. Acetone Wash Run 1-1	1	.1135 - .0002 <u>.1133</u>	67.3205 67.2153	.1135
S-74-001-702	"	F.H. H ₂ O Wash Run 1-1	2		68.1505 68.0797 <u>.0706</u>	
705(A)	"	B.H. H ₂ O Wash Run 1-1 (Organic Extract)	3		97.2231 99.2189 <u>.0042</u>	
S-74-000-706	"	B.H. Acetone Wash Run 1-1	4	.0194 - .0002 <u>.0192</u>	67.1897 67.1703 .0194	
705(B)	"	B.H. H ₂ O Remain Run 1-1	5		98.1176 97.9722 <u>.1387</u>	
S-74-000-711	"	F.H. Acetone Wash 1-2	6	.0836 - .0002 <u>.0834</u>	67.4935 67.4099 .0836	
S-74-000-710	"	F.H. H ₂ O Wash 1-2	7		68.2024 68.1552 <u>.0472</u>	
713(A)	"	B.H. H ₂ O Wash (Organic Extract)	8		101.1636 101.1601 <u>.0035</u>	
Case 708	+ .0002 / 742 + .0028					

67.2241

EPA No	Contract No	TYPE	Beaker No
S-74-000-714	337-9	BH. Acetone Wash Run 1-2.	Final 68.0939 Tare 68.0781 Gain .0158 <u>.0156</u>
713(B)	337-9	BH. H ₂ O Remain Run 1-2	10 101.8673 101.6835 <u>.1838</u>
S-74-000-739	337-9	FH. Acetone Wash Run 2-3	11 66.16502 66.5957 <u>.0545</u>
738	337-9	FH. H ₂ O Wash Run 2-3	12 66.3802 66.3632 <u>.0170</u>
74(A)	337-9 ✱	BH. H ₂ O Wash Organic Extract Run 2-3	13 102.9933 102.9549 <u>.0034</u>
741	337-9	BH. Acetone Wash Run 2-3	14 66.2552 66.2327 <u>.0225</u>
74(B)	337-9	H ₂ O Remain B.H. Run 2-3	15 98.3500 93.1377 <u>.2123</u>
746	337-9	FH. Acetone Wash Run 2-4	16 67.8319 67.7706 <u>.0613</u>

16	745	337-9	F.H. H ₂ O Wash Run 2-4	Rate 11.17 67.2142 67.1575 (.0272)
17	747 (A)	337-9 *	B.H. H ₂ O Wash Organic Extraction Run 2-4	18 105.5290 105.5-45 (.0045)
	748	337-9	B.H. Acetone Wash Run 2-4	19 (.0345) (.0022) (.0317) 67.7212 67.0367 .0345
	747 (B)	337-9	B.H. H ₂ O Remover Run 2-4	20 check 100.9240 100.7032 (.1207)
6	763	337-9	F.H. Acetone Wash Run 3-5	21 (.0683) (.0022) (.0655) 63.6037 63.5354 .0683
6	762	337-9	F.H. H ₂ O Wash Run 3-5	22 68.3845 68.3632 (.0213)
7	764 (A)	337-9 *	B.H. H ₂ O Wash (Organic Extn) Run 3-5	23 99.4570 99.4510 (.0060)
	765	337-9	B.H. Acetone Wash Run 3-5	24 (.0631) (.0028) (.0603) 66.7349 66.6718 .0631

764 (A)	337-9	BH H ₂ O Remain 3-5 Run	Baker No 25 102.8544 102.7525 <u>.0979</u>
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768	337-9	F.H. Acetone Wash Run 3-6	26 .0666 .0028 <u>.0638</u> 68.0016 67.9350 .0666
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767	337-9	F.H. H ₂ O Wash Run 3-6	27 68.1592 68.1352 <u>.0262</u>
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769 (A)	337-9 *	BH H ₂ O Wash Oxalic Extra Run 3-6	28 153.0330 153.0273 <u>.0052</u>
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770	337-9	B.H. Acetone Wash Run 3-6	29 .0250 .0028 <u>.0222</u> 66.6521 66.6271 .0250
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769 (B)	337-9	BH H ₂ O Remain Run 3-6	30 101.5031 101.2905 <u>.2126</u>
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John Deere Plant
Waterloo, Iowa C-337-7

5-74-001 001	337-7	F.H. Acetone Wash Run 3-6	31 Final 100.0210 Tare 100.0012 Gain .0198
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SILICA
GEL

755	232g	(Run - Filter 2-3 (5-100))
777	238g	3-5
726	221g	1-2
725	241g	1-1
778	237.5	3-6
756	227.0g	2-4

1	2	3	4	5	6
224.0	152.0	200.0	259.0	289.0	229.0
41.0	21.0	32.0	27.0	38.0	37.5
265.0	173.0	232.0	286.0	327.0	266.5

TABLE 2
NO_x METHOD 7 RESULTS*
MARBLEHEAD LIME CO.
GARY, IND.

<u>Date</u>	<u>Sample</u>	<u>µgms NO₂</u>
6/11/74	1 S-74-000 715	145.6
	2 716	132.0
	3 717	138.8
	4 718	146.7
6/12/74	5 749	143.1
	6 750	143.1
	7 751	118.1
	8 752	107.4
6/13/74	9 771	279.1
	10 772	221.9
	11 773	268.4
	12 774	225.5

*Method description followed was a draft procedure from L. Katzman

TABLE 4
 SO₂ METHOD 6 RESULTS
 MARBLEHEAD LIME CO.
 GARY, IND.

<u>Date</u>	<u>Sample</u>	<u>g - eg SO₂*</u>
6/11/74	1 S-74-000-719	0.379
	2 720	0.212
6/12/74	3 753	0.390
	4 754	0.327
6/13/74	5 775	0.375
	6 776	0.226

* Average of duplicate determinations on the same sample

Field Identification of NOx Samples

Description jars with Marburg tape labels:

Marburg NOx and numbered 1 → 15

Dated 1, 2 and 3 6/18/74

4 → 15 6/19/74

Description of jars with the EPA labels

Common to all labels "Marblehead Lime Co.

Gray Ind.

Method 7 NOx

Sample No.

1	26 ml	Bottle 7	6/11/74	S-74-000-715
2	24.5 ml	Bottle 8	6/11/74	S-74-000-716
3	24 ml	Bottle 9	6/11/74	S-74-000-717
4	25.5 ml	Bottle 10	6/11/74	S-74-000-718
5	25 ml		6/12/74	S-74-000-749
6	25 ml		6/12/74	S-74-000-750
7	25 ml		6/12/74	S-74-000-751
8	24 ml		6/12/74	S-74-000-752
9	26 ml		6/13/74	S-74-000-771
10	26 ml		6/13/74	S-74-000-772
11	25 ml		6/13/74	S-74-000-773
12	26 ml		6/13/74	S-74-000-774

SOx Identification

Common to all labels "Marblehead Lime

Gray Ind.

Method 6 SO₂

1	6/11/74	S-74-000-719
2	6/11/74	720
3	6/12/74	753
4	6/12/74	754
5	6/13/74	775
6	6/13/74	776

Marburg tape labels "SO₂ Impinger Wash
John Deere Waterloo Dura"

1	18 June 1974	Test No. 1
2	17 "	Test No. 2
3	19 "	Test No. 3
4	20 "	Test No. 4

7/3/74

SO₂ Samples

Note: Samples are greater than 50 only, as diluted to 100mL and 25mL taken for analysis.
20mL, 140mL IPA & 4 drops Thionin

Sample		20mL	Mls Ba(ClO ₄) ₂	mls Titrated	SO ₂ gm-%
6/11/74 Garg Ind	A		0.00 - 7.35	7.35	0.379
Sample #1 (715)	B		7.35 - 14.70	7.35	
6/11/74 Garg Ind		10 drop			
Sample #2 (500)	A		14.70 - 17.85	4.15	0.212
	B		17.85 - 22.95	4.10	
6/12/74 Garg Ind	A		22.95 - 30.51	7.56	0.390
Sample #3 (753)	B		30.51 - 38.10	7.59	
6/13/74 Garg Ind	A		38.15 - 44.42	6.27	0.327
Sample #4 (754)	B		44.42 - 50.69	6.27	
6/13/74 Garg Ind	A		0.65 - 6.65	6.00	0.375
Sample #5 (775)	B		6.65 - 12.70	6.05	
Blank		2 drop			
6/13/74 Garg Ind Sample	A		12.70 - 16.45	3.75	0.226
Sample #6 (776)	B		16.45 - 20.20	3.75	
6/13/74 Garg Ind	A		20.20 - 26.30	1.10	0.0528
Sample #7 (777)	B		26.30 - 31.30	0.95	
6/13/74 Garg Ind	A		31.30 - 32.25	0.95	0.0623
Sample #8 (778)	B		32.25 - 33.25	1.00	
6/13/74 Garg Ind	A		33.25 - 34.30	1.05	0.0521
Sample #9 (779)	B		34.30 - 35.13	0.83	
6/13/74 Garg Ind	A		35.13 - 35.00	0.87	0.0443
Sample #10 (780)	B		35.00 - 36.05	0.70	
6/13/74 Garg Ind	A		36.05 - 36.70	0.70	
Sample #11 (781)	B		36.70 - 37.40	0.70	
SO ₂ Blank	A				
Standard Dev	B				

$$N \text{ of } Ba(ClO_4)_2 = 0.0103$$

Eg 6.2 from Method 6

$$C_{SO_2} = \left(7.65 \times 10^{-5} \frac{\text{g}}{\text{mL}} \right) \frac{(V_t - V_{c8}) N \left(\frac{V_{std}}{V_t} \right)}{V_{std}}$$

7/1/74

NO₂ Samples

Samples: These samples were not made basic in the field. Samples of 6/18 and 6/19.

Procedure: Revised draft from Larry Katzman
(See Opposite Page)

1 ml = 25 µg

Sample	µgms NO ₂	U _{0.7}	A _{0.7}	Corrected Absorbance	K _c
0	0	98.5	0.005	0.0	$K_c = \frac{1.125 A_1 + 3.00 A_2 + 7.875 A_3 + 12.5 A_4}{A_1^2 + A_2^2 + A_3^2 + A_4^2}$ $= \frac{0.002 + 0.0036 + 0.0110 + 0.0121}{0.0348}$ $K_c = 732.76$
1 ml	25	89.5	0.05	A ₁ 0.045	
2	50	85.6	0.065	A ₂ 0.060	
3	75	77.0	0.11	A ₃ 0.105	
4	100	70.0	0.14	A ₄ 0.135	

Sample	µgms NO ₂	U _{0.7}	A _{0.7}	Corrected Absorbance	K _c
6/18/74 #1	91.0	0.040	0.035	25.7	$K_c = 100 \frac{0.5 A_1 + 1.32 A_2 + 2.36 A_3 + 4.43 A_4}{A_1^2 + A_2^2 + A_3^2 + A_4^2}$ $= \frac{0.0225 + 0.09 + 0.1736 + 0.3981}{0.6542}$ $K_c = 677.16$
#2	96.0	0.015	0.010	7.33	
#3	95.5	0.020	0.015	10.99	
6/19/74 #5	96.5	0.015	0.010	7.33	
#6	96.0	0.017	0.012	8.99	
#7	98.0	0.005	0.000		
#10	95.5	0.020	0.015	10.99	
#11	97.5	0.016	0.005	3.66	
#15	95.5	0.015	0.010	7.33	
#12	95.5	0.012	0.007	1.35	
#14	94.5	0.021	0.011	7.45	

Sample	µgms NO ₂	U _{0.7}	A _{0.7}	Corrected Absorbance	K _c
0	97.5	0.01	0.0		$K_c = 100 \frac{0.5 A_1 + 1.32 A_2 + 2.36 A_3 + 4.43 A_4}{A_1^2 + A_2^2 + A_3^2 + A_4^2}$ $= \frac{0.0225 + 0.09 + 0.1736 + 0.3981}{0.6542}$ $K_c = 677.16$
1 ml	69.0	0.16	A ₁ 0.15	100	
2	39.0	0.31	A ₂ 0.30	200	
3	35.5	0.45	A ₃ 0.44	300	
4	25.0	0.60	A ₄ 0.59	400	
6/17/74 #4	92.0	0.035	0.025	16.9	$K_c = 100 \frac{0.5 A_1 + 1.32 A_2 + 2.36 A_3 + 4.43 A_4}{A_1^2 + A_2^2 + A_3^2 + A_4^2}$ $= \frac{0.0225 + 0.09 + 0.1736 + 0.3981}{0.6542}$ $K_c = 677.16$
#8	94.0	0.025	0.015	10.2	
#9	97.0	0.040	0.030	20.3	
#12	98.0	0.010	0.000		
#13	97.0	0.012	0.002	1.35	
#14	94.5	0.021	0.011	7.45	
7/1/74 1	59.0	0.025	0.015	145.6	
2	62.0	0.205	0.195	132.0	
3	61.0	0.215	0.205	138.5	
4	92.5	0.010	0.000		

this block

7/3/74

Ind = 100 ug

Styrene

@ 410 nm

$T_{0.1}$	$A_{0.1}$
98.5	0.005
69.0	0.160
50.0	0.300
35.5	0.450
27.5	0.550

Subtracting the reagent blank of

66.0	0.215
60.0	0.213
61.5	0.210
67.0	0.175
69.0	0.166
40.0	0.463
42.0	0.320
41.0	0.345
47.0	0.325

Corrected Absorbance

$K_c = 100$

149 ug L_{0.2}

A_1	0.155	100
A_2	0.395	200
A_3	0.445	300
A_4	0.545	400

0.010 for 6/11 Samples

0.205	146.7
0.200	143.1
0.200	143.1
0.165	118.1
0.150	107.4
0.390	279.1
0.310	221.9
0.395	268.4
0.315	225.5

$K_c = 715.73$

4.24

2.13

$$A_1 + 2A_2 + 3A_3 + 4A_4$$

$$A_1^2 + A_2^2 + A_3^2 + A_4^2$$

0.0133 0.027 0.120 0.2970

0.5952

APPENDIX I

TEST LOG

SAMPLING TASK LOG

Plant Walden Lime Co.
Date 6-11-74

Plant Location Dary, Indiana
Recorded by _____

Comments	Run	Sampling location (port)	Pollutant	Clock Time Began	Elapsed Time (min)	Sample NOS.
Three stops due to power loss	1-1	Stack #1, NORTH	Particulate	12:25	120	S-74-000-701-703, 704-705, 715, 721
						"
						"
	"	" SOUTH	"	12:00	120	"
						"
Three stops due to power loss	1-2	Stack #2, NORTH	"	12:15	40	S-74-000-706-710, 713, 714, 716, 728
	"	"	"	12:20	20	"
	"	"	"	12:50	10	"
	"	"	"	14:10	50	"
	"	" SOUTH	"	12:00	120	"
	1	Stack #5, SOUTH	NOX	13:21	<1	S-74-000-715
	2	"	"	14:03	"	" 716
	3	"	"	16:15	"	" 717
	4	"	"	17:34	"	" 718
Three stops due to power loss	1	Stack #5	SO ₂	12:30	37	S-74-000-719
	"	"	"	13:10	7	"
	"	"	"	13:18	3	"
	"	"	"	13:28	4	"
Test stopped due to excessive impinger bubbling	2	"	"	14:00	30	S-74-000-720
	1		CO	15:00	120	
Material composite sample for one day		lime stone feed				S-74-000-721
"		blended coal				" 722
"		lime product				" 723
"		baghouse dust				" 724

SAMPLING TASK LOG

Plant Mobil Chemicals, Inc. Co.
Date 6-11-74

Plant Location Bay, Indiana
Recorded by

6/12/74

Comments	Run	Sampling location (Port)	Pollutant	Clock Time Begun	Clock Time Ended	Elapsed Time (min)	Sample Nos.
	2-3	Stack #3, South	Particulate	10:30	12:30	120	5-14-000-131-743, 727, 155
	"	" , NORTH	"	12:55	14:55	120	" "
	2-4	Stack #4, South	"	10:50	12:50	120	5-14-000-144-747, 120, 152
	"	" , NORTH	"	12:55	13:15	30	
	"	" "	"	13:15	13:45	10	
	"	" "	"	14:10	15:30	80	
	5	Stack #6, South	NOx	12:23	12:24	<1	5-14-000-749
	6	" "	"	13:05	13:10	"	" 750
	7	" "	"	13:42	13:41	"	" 751
	8	" "	"	14:14	14:15	"	" 752
	3	Stack #2	SO ₂	11:00	11:40	40	5-14-000-753
	4	"	"	13:50	14:30	40	" 754
	2		CO	10:30	12:30	120	
	2	limestone fuel					5-14-000-755
	"	submerged coal					" 754
	"	lime product					" 755
	"	baghouse dust					" 756
	3-5	Stack #5, South	Particulate	09:30	11:30	120	5-14-000-761-765, 151, 177
	"	" , South	"	11:00	14:00	180	" "
	3-6	Stack #6, North	"	09:30	11:30	120	5-14-000-766-770, 152, 178
	"	" , South	"	11:00	14:00	180	" "
			NOx				5-14-000-743

Mixed, composite sample for one day

"

"

"

6/13/74

NOx Absorption Solution Blank

NY