

Note: This is a reference cited in *AP 42, Compilation of Air Pollutant Emission Factors, Volume I Stationary Point and Area Sources*. AP42 is located on the EPA web site at www.epa.gov/ttn/chief/ap42/

The file name refers to the reference number, the AP42 chapter and section. The file name "ref02_c01s02.pdf" would mean the reference is from AP42 chapter 1 section 2. The reference may be from a previous version of the section and no longer cited. The primary source should always be checked.

Background Report Reference

AP-42 Section Number: 11.23

Background Chapter: 4

Reference Number: 50

Title: Results of the January 10-13, 1995 Air
Emission Compliance Testing at teh
Northshore Mining Facility in Silver
Bay, MN

Interpoll Laboratories, IncInterpoll
Laboratories, Inc

Interpoll Laboratories, IncInterpoll
Laboratories, Inc

January 1995

27A
Interpoll Laboratories, Inc.
4500 Ball Road N.E.
Circle Pines, Minnesota 55014-1819

TEL: (612) 786-6020
FAX: (612) 786-7854

AP-42 Section 1123
Reference -
Report Sect. 4
Reference 50

Ref 4-50

**RESULTS OF THE JANUARY 10 - 13, 1995
AIR EMISSION COMPLIANCE TESTING AT THE
NORTHSHORE MINING FACILITY IN
SILVER BAY, MINNESOTA**

Submitted to:

NORTHSHORE MINING COMPANY
10 Outer Drive
Silver Bay, Minnesota 55614

Attention:

Dennis Wagner

Approved by:



Daniel Despen
Manager
Stationary Source Testing Department

Report Number 5-4664
January 25, 1995
SP/slp



Northshore Mining Company
A Subsidiary of Cliffs Minnesota Minerals Company

February 28, 1995

Mr. Stuart Arkley
Division of Air Quality
Minnesota Pollution Control Agency
520 Lafayette Road
St. Paul, MN 55155



Re: Northshore Mining Company
Compliance Re-testing
Week of January 9, 1995

Dear Mr. Arkley:

Enclosed is the Interpoll Report Number 5-4664 entitled "Results of the January 10-13, 1995 Air Emission Compliance Testing at the Northshore Mining Facility in Silver Bay, Minnesota." Due to a communications mix-up, operating data was not included in the report. Northshore will obtain this information from our operating records and submit it under separate cover. In the interim and for the purposes of your initial review, the following preliminary operating information is provided:

Fine Crusher feed rate - 350 to 605 LTPH.
Dry Cobber feed rate - 1052 to 1814 LTPH.
Concentrator bin feed rate - 175 to 200 LTPH.
Furnace 11 WWESP's - 277 LTPH.
Furnace 12 WWESP's - 270 LTPH.
Furnace 12 Rotoclone - 270 LTPH.
Power Boiler #2 - 70 to 78 MW/Hr (75.8 Ave.).
Power Boiler #2 Firing coal.

As soon as I receive the rest of the operating data from Interpoll, I will submit the completed operating data summary forms to the Agency. The enclosed report has been sent out for microfiche and the microfiche will be forwarded to the Agency as soon as returned. Contact me at 218/226-6056 if you have any questions.

Sincerely,

A handwritten signature in cursive script that reads 'Dennis M. Wagner'.

Dennis M. Wagner
Sr. Environmental Engineer

DMW/pr

Encl.

B. Analysis of the performance test indicates that the following has been demonstrated:

REV/YH/93

Pollutant

PM

Limitation Basis or Applicable Rule: S.C. II. A.I. of the Permit
Limit: 0.03 gr/dscf
Measured Emissions (Units of measurement 0.0055 gr/dscf):
Run 1 _____ Run 2 _____ Run 3 _____
Average 0.0055

Compliance (circle one): YES NO CANNOT DETERMINE

PM

Limitation Basis or Applicable Rule: S.C. II. A.I. of the Permit
Limit: 0.01
Measured Emissions (Units of measurement gr/dscf):
Run 1 _____ Run 2 _____ Run 3 _____
Average 0.011

Compliance (circle one): YES NO CANNOT DETERMINE

PM

Limitation Basis or Applicable Rule: S.C. II. A.I. of the Permit
Limit: 0.01
Measured Emissions (Units of measurement gr/dscf):
Run 1 _____ Run 2 _____ Run 3 _____
Average 0.009

Compliance (circle one): YES NO CANNOT DETERMINE

PM

Limitation Basis or Applicable Rule: S.C. II. A.I. of the Permit
Limit: 0.01
Measured Emissions (Units of measurement gr/dscf):
Run 1 _____ Run 2 _____ Run 3 _____
Average 0.011

Compliance (circle one): YES NO CANNOT DETERMINE

SO₂

Limitation Basis or Applicable Rule: Test Required by Permit
Limit: N/A
Measured Emissions (Units of measurement _____):
Run 1 _____ Run 2 _____ Run 3 _____
Average _____

Compliance (circle one): YES NO CANNOT DETERMINE

NO_x

Limitation Basis or Applicable Rule: _____
Limit: _____
Measured Emissions (Units of measurement _____):
Run 1 _____ Run 2 _____ Run 3 _____
Average _____

Compliance (circle one): YES NO CANNOT DETERMINE

BIN Storage
Stack
(EP# 48)1105 Pelletizer
Waste Stack
(EP# 105)1104 Pelletizer
Waste Stack
(EP# 104)Solid No. 12
1205 Waste Gas
Stack
(EP# 107)1205 Waste
Gas Stack1205 Waste Gas
Stack

B. Analysis of the performance test indicates that the following has been demonstrated:

REV/YH/93

Pollutant

PM

1204 WASTE
GAS STACK

(EP# 106)

Limitation Basis or Applicable Rule: _____

Limit: _____

Measured Emissions (Units of measurement _____):

Run 1 _____ Run 2 _____ Run 3 _____

Average _____

Compliance (circle one): YES NO CANNOT DETERMINE

PM

Rotoclone Stack

(EP# 76)

Limitation Basis or Applicable Rule: _____

Limit: _____

Measured Emissions (Units of measurement _____):

Run 1 _____ Run 2 _____ Run 3 _____

Average _____

Compliance (circle one): YES NO CANNOT DETERMINE

PM

No. 2 Boiler
STACK

(EP# 2)

Limitation Basis or Applicable Rule: _____

Limit: _____

Measured Emissions (Units of measurement _____):

Run 1 _____ Run 2 _____ Run 3 _____

Average _____

Compliance (circle one): YES NO CANNOT DETERMINE

SO₂

No. 2 Boiler
STACK

(EP NO. 2)

Limitation Basis or Applicable Rule: _____

Limit: _____

Measured Emissions (Units of measurement _____):

Run 1 _____ Run 2 _____ Run 3 _____

Average _____

Compliance (circle one): YES NO CANNOT DETERMINE

PM

Fine Crusher
STACK

(EP# 11)

Limitation Basis or Applicable Rule: _____

Limit: _____

Measured Emissions (Units of measurement _____):

Run 1 _____ Run 2 _____ Run 3 _____

Average _____

Compliance (circle one): YES NO CANNOT DETERMINE

PM

Dry Cobber Stack

(EP# 22)

Limitation Basis or Applicable Rule: _____

Limit: _____

Measured Emissions (Units of measurement _____):

Run 1 _____ Run 2 _____ Run 3 _____

Average _____

Compliance (circle one): YES NO CANNOT DETERMINE

B. Analysis of the performance test indicates that the following has been demonstrated:

REV/YH/93

Pollutant

Limitation Basis or Applicable Rule: _____

Limit: _____

Measured Emissions (Units of measurement _____):

Run 1 _____ Run 2 _____ Run 3 _____

Average _____

Compliance (circle one): YES NO CANNOT DETERMINE

Limitation Basis or Applicable Rule: _____

Limit: _____

Measured Emissions (Units of measurement _____):

Run 1 _____ Run 2 _____ Run 3 _____

Average _____

Compliance (circle one): YES NO CANNOT DETERMINE

Limitation Basis or Applicable Rule: _____

Limit: _____

Measured Emissions (Units of measurement _____):

Run 1 _____ Run 2 _____ Run 3 _____

Average _____

Compliance (circle one): YES NO CANNOT DETERMINE

Limitation Basis or Applicable Rule: _____

Limit: _____

Measured Emissions (Units of measurement _____):

Run 1 _____ Run 2 _____ Run 3 _____

Average _____

Compliance (circle one): YES NO CANNOT DETERMINE

Limitation Basis or Applicable Rule: _____

Limit: _____

Measured Emissions (Units of measurement _____):

Run 1 _____ Run 2 _____ Run 3 _____

Average _____

Compliance (circle one): YES NO CANNOT DETERMINE

Limitation Basis or Applicable Rule: _____

Limit: _____

Measured Emissions (Units of measurement _____):

Run 1 _____ Run 2 _____ Run 3 _____

Average _____

Compliance (circle one): YES NO CANNOT DETERMINE

METHOD PM			Test No. 2	Test Date(s) 1/10/95						
Run No. 1			AQD File 27A							
			Unit tested: 1105 Pelletizer							
Nozzle diameter	Dn	0.247	inches	A(stack)	27.49	I	0 inches	sum sqrt	24	0.924214
Stack Diameter	Ds	#DIV/0!	inches	D(stack)	70.99433	w	0 inches			
Area of nozzle	Area n	0.000333	square feet			De	#DIV/0!	inches	1.05	1.024695
Area of stack	Area s	27.49	square feet			As	0 sq ft		0.97	0.984886
time of run	theta	60	minutes						1	1
meter coefficient	gamma	1.0015	unitless						1	1
volume of water in impingers	Vwc	167	ml	front mass	3.07E-02 grams				0.96	0.979796
volume of water in silica gel	Vwsg	24	grams	back mass	0.0036 grams				0.95	0.974679
	Vwc,std	7.86069	scf	total mass	0.0343 grams				0.97	0.984886
	Vwsg,std	1.1316	scf	front C	0.00916215 gr/dscf				0.82	0.905539
Moisure content of gas	Bws	0.148157	fraction	front C	1.3089E-06 lb/dscf				0.77	0.877496
vol of gas as measured by dry gas meter	Vm	53.6	dcf	front C	5.52224788 lb/hr				0.55	0.74162
pilot tube coefficient	Cp	0.84		back C	0.00107439 gr/dscf				0.5	0.707107
pilot tube constant	Kp	85.49	*const	back C	1.5348E-07 lb/dscf				0.48	0.69282
Stack temperature (F +460)	Ts	588	R	back C,lb/hr	0.64756001 lb/hr				0.6	0.774597
Meter temperature (F+460)	Tm	541.8	R	total C	0.01023654 gr/dscf				0.79	0.888819
baometric pressure	Pb	29.38	in Hg	total C	1.4624E-06 lb/dscf				0.92	0.959166
static pressure	Pg	-0.22	in H2O	total C	6.1698079 lb/hr				0.96	0.979796
Absolute stack gas pressure	Ps	29.36382353	in Hg	total C	0.02344586 grams/dscm				0.96	0.979796
ave press diff across orifice meter	dela H	2.59	inches	total C	663.912704 microgram/dscf				0.97	0.984886
ave of square root della p's	dclap	0.924214	inch	total C	23.4458555 mg/dscm				0.94	0.969536
Stack gas velocity	Vs	56.79005	f/s	Uncorrected					0.95	0.974679
Stack gas volumetric flow rate	Qa	93669.5	acfm	at 7%O2	#VALUE!				0.96	0.979796
Stack gas dry volumetric flow rate	Qsd	70317.8	dscfm	at 12%CO2	#VALUE!				0.95	0.974679
	Vmsld	51.70194							0.93	0.964365
Wet molecular weight	Ms	27.34983							0.77	0.877496
	%CO2	1.8							0	0
	%O2	17.2							0	0
	%N2	81							0	0
	%CO	0							0	0
Dry molecular weight	Md	28.976							0	0
	%EA	411.0899							0	0
CONCENTRATION FROM F FACTOR For Total										
F-factor	dscf/mmbtu		Front Only						0	0
C	1E-06 lb/dscf		1.31E-06 lb/dscf						0	0
Fo	2.0556		0 lb/mmbtu						0	0
E*	0 lb/mmbtu		Back Only						0	0
I intermediate values	101.3 %		1.53E-07 lb/dscf						0	0
I raw	99.359 %		0 lb/mmbtu						0	0

METHOD PM

Test No. 1
Run No. 1Test Date(s) 1/10/95
AQD File 27A

Unit tested: Bin Storage

sqft avg dp

1.004695

counter

24

Nozzle diameter
Dn 0.186 inches

A(stack)

8.51

1 0 inches

sum sqft

24.11268

Stack Diameter
Ds #DIV/OI inches

D(stack)

39.50036

w 0 inches

0.9

0.948683

Area of nozzle
Area n 0.000189 square feet

D(stack)

39.50036

De #DIV/OI inches

1

1

Area of stack
Area s 8.51 square feet

D(stack)

39.50036

As 0 sq ft

1.1

1.048809

time of run
theta 60 minutes

D(stack)

39.50036

As 0 sq ft

1.1

1.048809

meter coefficient
gamma 1.0004 unitless

D(stack)

39.50036

As 0 sq ft

1.15

1.072381

volume of water in impingers
Vwc 0 ml

D(stack)

39.50036

As 0 sq ft

1.15

1.072381

volume of water in silica gel
Vwsg 8 grams

D(stack)

39.50036

As 0 sq ft

1.15

1.072381

Vwc, std 0 scf

D(stack)

39.50036

As 0 sq ft

1.1

1.048809

Vwsg, std 0.3772 scf

D(stack)

39.50036

As 0 sq ft

1.12

1.058301

Moisture content of gas
Bws 0.00985 fraction

D(stack)

39.50036

As 0 sq ft

1.1

1.048809

vol of gas as measured by dry gas meter
Vm 37.83 def

D(stack)

39.50036

As 0 sq ft

1.1

1.048809

pilot tube coefficient
Cp 0.84

D(stack)

39.50036

As 0 sq ft

1.05

1.024695

pilot tube constant
Kp 85.49

D(stack)

39.50036

As 0 sq ft

0.85

0.921954

Stack temperature (F +460)
Ts 518

D(stack)

39.50036

As 0 sq ft

0.65

0.806226

Meter temperature (F+460)
Tm 520.5

D(stack)

39.50036

As 0 sq ft

0.7

0.83666

barometric pressure
Pg -0.65

D(stack)

39.50036

As 0 sq ft

0.75

0.866025

static pressure
Ps 29.41220588

D(stack)

39.50036

As 0 sq ft

0.85

0.921954

Absolute stack gas pressure
delta H 1.23

D(stack)

39.50036

As 0 sq ft

1.1

1.048809

ave press diff across orifice meter
delap 1.004695

D(stack)

39.50036

As 0 sq ft

1.15

1.072381

ave of square root delta p's
Vs 56.48481 ft/s

D(stack)

39.50036

As 0 sq ft

1.15

1.072381

Stack gas velocity
Qa 28841.14 acfm

D(stack)

39.50036

As 0 sq ft

1.1

1.048809

Stack gas volumetric flow rate
Qsd 28614.33 dscfm

D(stack)

39.50036

As 0 sq ft

1.1

1.048809

Stack gas dry volumetric flow rate
Vmsid 37.91627

D(stack)

39.50036

As 0 sq ft

1.05

1.024695

Wet molecular weight
Ms 28.73402

D(stack)

39.50036

As 0 sq ft

0.95

0.974679

%CO2 0.03

D(stack)

39.50036

As 0 sq ft

0

%O2 20.9

D(stack)

39.50036

As 0 sq ft

0

%N2 79.07

D(stack)

39.50036

As 0 sq ft

0

%CO 0

D(stack)

39.50036

As 0 sq ft

0

MD 28.8408

D(stack)

39.50036

As 0 sq ft

0

%EA -81896.55

D(stack)

39.50036

As 0 sq ft

0

Dry molecular weight

D(stack)

39.50036

As 0 sq ft

0

CONCENTRATION FROM F FACTOR For Total

D(stack)

39.50036

As 0 sq ft

0

F-factor

D(stack)

39.50036

As 0 sq ft

0

C

D(stack)

39.50036

As 0 sq ft

0

Fo

D(stack)

39.50036

As 0 sq ft

0

E*

D(stack)

39.50036

As 0 sq ft

0

#DIV/OI lb/mmbtu

D(stack)

39.50036

As 0 sq ft

0

#DIV/OI lb/dscf

D(stack)

39.50036

As 0 sq ft

0

I intermediate values

D(stack)

39.50036

As 0 sq ft

0

I raw

D(stack)

39.50036

As 0 sq ft

0

METHOD		PM	Test No. 3	Test Date(s) 1/10/95	AOD File 27A		Unit tested: 1104 Pelletizer	sqrt avg dp	0.915886
		Run No. 1						counter	24
Nozzle diameter	Dn	0.25	inches	A(stack)	27.49	I	0 inches	sum sqrt	21.98125
Stack Diameter	Ds	#DIV/0!	inches	D(stack)	70.99433	w	0 inches		1.095445
Area of nozzle	Area n	0.000341	square feet			De	#DIV/0!		1.2
Area of stack	Area s	27.49	square feet			As	0 sq ft		1.095445
time of run	theta	60	minutes						1
meter coefficient	gamma	0.9932	unitless						0.88
volume of water in impingers	Vwc	172	ml						0.938083
volume of water in silica gel	Vwsg	20	grams						0.6
	Vwc,std	8.09604	scf						0.774597
	Vwsg,std	0.943	scf						0.49
Moisture content of gas	Bws	0.149799	fraction						1.2
vol of gas as measured by dry gas meter	Vm	53.32	dcf						1.095445
pilot tube coefficient	Cp	0.84							1
pilot tube constant	Kp	85.49	*const						0.85
Stack temperature (F +460)	Ts	592	R						0.921954
Meter temperature (F+460)	Tm	538.4	R						0.44
barometric pressure	Pb	29.38	in Hg						0.663325
static pressure	Pg	-0.14	in H2O						1.1
Absolute stack gas pressure	Ps	29.36970588	in Hg						1.048809
ave press diff across orifice meter	della H	2.39	inches						1.1
ave of square root delta p's	dellap	0.915886	inch						1.048809
Stack gas velocity	Vs	56.46829	f/s						1
Stack gas volumetric flow rate	Qa	93138.8	acfm						0.89
Stack gas dry volumetric flow rate	Qsd	69327.03	dscfm						0.65
	Vmsid	51.30219							0.79
	Ms	27.34541							0.83666
Wet molecular weight	%CO2	1.9							0.69
	%O2	17.2							0.75
	%N2	80.9							0.866025
	%CO	0							0.64
Dry molecular weight	Md	28.992							0.52
	%EA	413.7002							0.72111
CONCENTRATION FROM F FACTOR For Total									
F-factor		dscf/mmbtu	Front Only						0
C	2E-06	lb/dscf	1.62E-06	lb/dscf					0
Fo	1.9474			0 lb/mmbtu					0
E*		0 lb/mmbtu	Back Only						0
I intermediate values	99.519	%	5.59E-08	lb/dscf					0
I raw	97.914	%		0 lb/mmbtu					0

METHOD PM

Test No. 4
Run No. 1

Test Date(s) 1/11/95

AQD File 27A

Unit tested: 1205 Waste Gas

sqrt avg dp

0.853607

counter

24

sum sqrt

0.65

Nozzle diameter
Dn 0.247 inches
Area of nozzle
Ds #DIV/OI 0.000333 square feet
Area of stack
Area s 27.88 square feet
time of run
theta 60 minutes
meter coefficient
gamma 1.0015 unitless
volume of water in impingers
Vwc 127 ml
volume of water in silica gel
Vwsg 21 grams
Vwsg, std 5.97789 scf
Vwsg, std 0.99015 scf
Moisture content of gas
Bws 0.1316 fraction
vol of gas as measured by dry gas meter
Vm 47.33 dcf
pilot tube coefficient
Cp 0.84
pilot tube constant
Kp 85.49 *const
Stack temperature (F +460)
Ts 598 R
Meter temperature (F+460)
Tm 530.6 R
barometric pressure
Pb 29.02 in Hg
static pressure
Pg -0.03 in H2O
Absolute stack gas pressure
Ps 29.01779412 in Hg
ave press diff across orifice meter
delta H 1.99 inches
ave of square root delta p's
delta p 0.853607 inch
Stack gas velocity
Vs 53.00738 ft/s
Stack gas volumetric flow rate
Qa 88670.75 acfm
Stack gas dry volumetric flow rate
Qsd 65937.99 dscfm
Wet molecular weight
Ms 45.98056
%CO2 27.55935
%O2 2.1
%N2 16.8
%CO 81.1
%EA 0
Md 29.008
%EA 364.3935
Dry molecular weight
29.008
CONCENTRATION FROM F FACTOR For Total
F-factor dscf/rmbtu Front Only
C 1E-06 lb/dscf 1.23E-06 lb/dscf
Fo 1.9524 0 lb/rmbtu
E* 0 lb/rmbtu Back Only
I intermediate values 97.435 % 1.92E-07 lb/dscf
I raw 95.564 % 0 lb/rmbtuA(stack)
D(stack)27.88
71.496161
W
De #DIV/OI 0 inches
As 0 sq ftfront mass
back mass
total mass2.57E-02 grams
0.004 grams
0.0297 grams0.00862432 gr/dscf
1.232E-06 lb/dscf
4.87431622 lb/hr0.65 0.806226
0.67 0.818535
0.7 0.83666
0.74 0.860233
0.82 0.905539
0.9 0.948683
0.88 0.938083
0.83 0.911043
0.78 0.883176
0.67 0.818535
0.58 0.761577
0.49 0.7
0.62 0.787401
0.69 0.830662
0.69 0.830662
0.82 0.905539
0.94 0.969536
0.94 0.969536
0.85 0.921954
0.87 0.932738
0.74 0.860233
0.62 0.787401
0.6 0.774597
0.53 0.728011back C
back C
back C, lb/hr0.00996663 gr/dscf
1.4238E-06 lb/dscf
5.63296465 lb/hr0.02282764 grams/dscm
646.406855 micrograms/dscf
22.8276423 mg/dscm0.00996663 gr/dscf
1.4238E-06 lb/dscf
5.63296465 lb/hr0.00996663 gr/dscf
1.4238E-06 lb/dscf
5.63296465 lb/hrUncorrected
at 7%O2
at 12%CO2#VALUE!
#VALUE!
#VALUE!0.00996663 gr/dscf
1.4238E-06 lb/dscf
5.63296465 lb/hr0.02282764 grams/dscm
646.406855 micrograms/dscf
22.8276423 mg/dscm0.00996663 gr/dscf
1.4238E-06 lb/dscf
5.63296465 lb/hr0.00996663 gr/dscf
1.4238E-06 lb/dscf
5.63296465 lb/hr0.02282764 grams/dscm
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22.8276423 mg/dscm0.00996663 gr/dscf
1.4238E-06 lb/dscf
5.63296465 lb/hr0.00996663 gr/dscf
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1.4238E-06 lb/dscf
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646.406855 micrograms/dscf
22.8276423 mg/dscm0.00996663 gr/dscf
1.4238E-06 lb/dscf
5.63296465 lb/hr0.00996663 gr/dscf
1.4238E-06 lb/dscf
5.63296465 lb/hr0.02282764 grams/dscm
646.406855 micrograms/dscf
22.8276423 mg/dscm0.00996663 gr/dscf
1.4238E-06 lb/dscf
5.63296465 lb/hr0.02282764 grams/dscm
646.406855 micrograms/dscf
22.8276423 mg/dscm0.00996663 gr/dscf
1.4238E-06 lb/dscf
5.63296465 lb/hr0.00996663 gr/dscf
1.4238E-06 lb/dscf
5.63296465 lb/hr0.02282764 grams/dscm
646.406855 micrograms/dscf
22.8276423 mg/dscm0.00996663 gr/dscf
1.4238E-06 lb/dscf
5.63296465 lb/hr0.02282764 grams/dscm
646.406855 micrograms/dscf
22.8276423 mg/dscm0.00996663 gr/dscf
1.4238E-06 lb/dscf
5.63296465 lb/hr0.00996663 gr/dscf
1.4238E-06 lb/dscf
5.63296465 lb/hr0.02282764 grams/dscm
646.406855 micrograms/dscf
22.8276423 mg/dscm0.00996663 gr/dscf
1.4238E-06 lb/dscf
5.63296465 lb/hr0.02282764 grams/dscm
646.406855 micrograms/dscf
22.8276423 mg/dscm0.00996663 gr/dscf
1.4238E-06 lb/dscf
5.63296465 lb/hr0.00996663 gr/dscf
1.4238E-06 lb/dscf
5.63296465 lb/hr0.02282764 grams/dscm
646.406855 micrograms/dscf
22.8276423 mg/dscm0.00996663 gr/dscf
1.4238E-06 lb/dscf
5.63296465 lb/hr0.02282764 grams/dscm
646.406855 micrograms/dscf
22.8276423 mg/dscm0.00996663 gr/dscf
1.4238E-06 lb/dscf
5.63296465 lb/hr0.00996663 gr/dscf
1.4238E-06 lb/dscf
5.63296465 lb/hr0.02282764 grams/dscm
646.406855 micrograms/dscf
22.8276423 mg/dscm0.00996663 gr/dscf
1.4238E-06 lb/dscf
5.63296465 lb/hr0.02282764 grams/dscm
646.406855 micrograms/dscf
22.8276423 mg/dscm0.00996663 gr/dscf
1.4238E-06 lb/dscf
5.63296465 lb/hr0.00996663 gr/dscf
1.4238E-06 lb/dscf
5.63296465 lb/hr0.02282764 grams/dscm
646.406855 micrograms/dscf
22.8276423 mg/dscm0.00996663 gr/dscf
1.4238E-06 lb/dscf
5.63296465 lb/hr0.02282764 grams/dscm
646.406855 micrograms/dscf
22.8276423 mg/dscm0.00996663 gr/dscf
1.4238E-06 lb/dscf
5.63296465 lb/hr0.00996663 gr/dscf
1.4238E-06 lb/dscf
5.63296465 lb/hr0.02282764 grams/dscm
646.406855 micrograms/dscf
22.8276423 mg/dscm0.00996663 gr/dscf
1.4238E-06 lb/dscf
5.63296465 lb/hr0.02282764 grams/dscm
646.406855 micrograms/dscf
22.8276423 mg/dscm0.00996663 gr/dscf
1.4238E-06 lb/dscf
5.63296465 lb/hr

METHOD PM

Test No. 5
Run No. 1

Test Date(s) 1/11/95
AQD File 27A
Unit tested: 1204 Waste Gas

sqrt avg dp
counter
sum sqrt

Dn 0.25 inches

Ds #DIV/OI inches

Area n 0.000341 square feet

Area s 27.88 square feet

theta 60 minutes

gamma 0.9932 unitless

Vwc 205 ml

Vwsg 13 grams

Vwcstd 9.64935 scf

Vwsgstd 0.61295 scf

Bws 0.180323 fraction

Vm 47.98 dcf

Cp 0.84

Kp 85.49

Ts 600

Tm 525.7

Pb 29.02 in Hg

Pg 0.26 in H2O

Ps 29.03911765 in Hg

delta H 1.92 inches

delap 0.866741 inch

Vs 54.43854 ft/s

Qa 91064.79 acfm

Qsd 63752.58 dscfm

Vmsid 46.64836

Ms 27.00989

%CO2 2

%O2 16.8

%N2 81.2

%CO 0

Md 28.992

%EA 362.3188

A(stack) 27.88

D(stack) 71.49616

front mass 2.31E-02 grams

back mass 0.0009 grams

total mass 0.024 grams

front C 0.00764085 gr/dscf

front C 1.0915E-06 lb/dscf

front C 4.17534627 lb/hr

back C 0.0002977 gr/dscf

back C 4.2528E-08 lb/dscf

back C 0.16267583 lb/hr

total C 0.00793854 gr/dscf

total C 1.1341E-06 lb/dscf

total C 4.3380221 lb/hr

total C 0.01818251 grams/dscm

total C 514.871234 micrograms/dscf

total C 18.1825058 mg/dscm

Uncorrected at 7%O2

at 12%CO2

#VALUEI

#VALUEI

#VALUEI

#VALUEI

#VALUEI

#VALUEI

#VALUEI

#VALUEI

#VALUEI

#VALUEI

#VALUEI

#VALUEI

#VALUEI

0.866741

24

20.80178

0.95

0.974679

0.96

0.979796

0.9

0.948683

0.8

0.894427

0.7

0.83666

0.57

0.754983

0.95

0.974679

0.88

0.938083

0.72

0.848528

0.65

0.806226

0.6

0.774597

0.48

0.69282

0.9

0.948683

0.85

0.921954

0.7

0.83666

0.64

0.74162

0.5

0.707107

0.95

0.974679

0.94

0.969536

0.85

0.921954

0.78

0.883176

0.75

0.866025

0.65

0.806226

0

0

0

0

0

0

0

0

0

0

0

0

0

0

0

0

0

0

0

0

0

METHOD PM

Test No. 6

Test Date(s) 1/12/95

Run No. 1

AQD File 27A

Unit tested: Rotolone Stack

sqrt avg dp

1.01214

counter

20

sum sqrt

0.74

0.74

0.860233

0.98

0.989949

1.1

1.048809

1.3

1.140175

1.2

1.095445

1.3

1.140175

1.1

1.048809

1

1

1

1

0.85

0.921954

0.72

0.848528

0.94

0.969536

1.2

1.095445

1.3

1.140175

1.4

1.183216

1.2

1.095445

0.98

0.989949

0.97

0.984886

0.85

0.921954

0.59

0.768115

Dn 0.185 inches

Ds 45.49705 inches

Area n 0.000187 square feet

Area s 11.29 square feet

theta 60 minutes

gamma 0.9932 unitless

Vwc 33 ml

Vwsg 10 grams

Vwsgstd 1.55331 scf

Vwsgstd 0.4715 scf

Bws 0.061028 fraction

Vm 32.67 dcf

Cp 0.84

Kp 85.49

Ts 597

Tm 533.1

Pb 28.94

Pg -0.82

Ps 28.87970588

delta H 0.87

delap 1.01214

Vs 62.25817

Qa 42173.68

Qsd 33805.31

Vmsid 31.15351

Ms 28.1747

%CO2 0

%O2 20.9

%N2 79.1

%CO 0

Md 28.836

%EA -118750

1E-06 lb/dscf

#DIV/OI lb/rmbtu

#DIV/OI lb/rmbtu

92.95 %

91.578 %

A(stack) 11.29

D(stack) 45.49705

w 0

De #DIV/OI 0

As 0 sq ft

1.53E-02 grams

0.0005 grams

0.0158 grams

0.00757793 gr/dscf

1.0826E-06 lb/dscf

2.19577835 lb/hr

0.00024764 gr/dscf

3.5378E-08 lb/dscf

0.07175746 lb/hr

0.00782557 gr/dscf

1.1179E-06 lb/dscf

2.26753581 lb/hr

0.01792375 grams/dscm

507.544205 microgram/dscf

17.9237542 mg/dscm

Uncorrected

at 7%O2

at 12%CO2

#VALUE!

#VALUE!

#VALUE!

#VALUE!

#VALUE!

#VALUE!

#VALUE!

#VALUE!

#VALUE!

#VALUE!

#VALUE!

#VALUE!

#VALUE!

#VALUE!

METHOD PM

Test No. 7
Run No. 1

Test Date(s) 1/12/95

AQD File 27A

Unit tested: No.2 Boiler

sqrt avg dp 1.048106

counter 24

sum sqrt 1.15

1.05 1.024695

1.2 1.095445

1.2 1.095445

1.25 1.118034

1.25 1.118034

1.3 1.140175

1.35 1.161895

1.25 1.118034

1.1 1.048809

0.93 0.964365

0.95 0.974679

1.08 1.03923

1.03 1.014889

1.02 1.00995

1.03 1.014889

1.04 1.019804

1.04 1.019804

1.04 1.019804

1.04 1.019804

1.04 1.019804

1.04 1.019804

1.04 1.019804

1.01 1.004988

0

0

0

0

0

0

0

0

0

0

0

0

0

0

I 0 inches

W 0 inches

De #DIV/OI inches

As 0 sq ft

3.32E-02 grams

0.001 grams

0.0342 grams

front mass

back mass

total mass

0.00977372 gr/dscf

1.3962E-06 lb/dscf

14.3455687 lb/hr

0.00029439 gr/dscf

4.2056E-08 lb/dscf

0.43209544 lb/hr

0.01006811 gr/dscf

1.4383E-06 lb/dscf

14.7776641 lb/hr

0.02306009 grams/dscm

652.989045 microgram/dscf

23.0600902 mg/dscm

total C

total C

total C

total C

total C

total C

total C

total C

total C

total C

total C

total C

total C

total C

total C

total C

total C

A(stack)

D(stack)

110.0039

66

square feet

square feet

minutes

unilless

ml

grams

scf

scf

fraction

def

0.096568

0.096568

54.26

0.84

85.49

761

533.6

28.94

-0.9

28.87382353

2.62

1.048106

71.48618

283085.3

171239.7

52.4136

29.21701

13.7

5.6

80.7

0

30.416

35.65789

%EA

%EA

METHOD PM

Test No. 7
Run No. 1

Test Date(s) 1/12/95

AQD File 27A

Unit tested: No.2 Boiler

sqrt avg dp 1.048106

counter 24

sum sqrt 1.15

1.05 1.024695

1.2 1.095445

1.2 1.095445

1.25 1.118034

1.25 1.118034

1.3 1.140175

1.35 1.161895

1.25 1.118034

1.1 1.048809

0.93 0.964365

0.95 0.974679

1.08 1.03923

1.03 1.014889

1.02 1.00995

1.03 1.014889

1.04 1.019804

1.04 1.019804

1.04 1.019804

1.04 1.019804

1.04 1.019804

1.04 1.019804

1.04 1.019804

1.01 1.004988

0

0

0

0

0

0

0

0

0

0

0

0

0

0

I 0 inches

W 0 inches

De #DIV/OI inches

As 0 sq ft

3.32E-02 grams

0.001 grams

0.0342 grams

front mass

back mass

total mass

0.00977372 gr/dscf

1.3962E-06 lb/dscf

14.3455687 lb/hr

0.00029439 gr/dscf

4.2056E-08 lb/dscf

0.43209544 lb/hr

0.01006811 gr/dscf

1.4383E-06 lb/dscf

14.7776641 lb/hr

0.02306009 grams/dscm

652.989045 microgram/dscf

23.0600902 mg/dscm

total C

total C

total C

total C

total C

total C

total C

total C

total C

total C

total C

total C

total C

total C

total C

total C

total C

A(stack)

D(stack)

110.0039

66

square feet

square feet

minutes

unilless

ml

grams

scf

scf

fraction

def

0.096568

0.096568

54.26

0.84

85.49

761

533.6

28.94

-0.9

28.87382353

2.62

1.048106

71.48618

283085.3

171239.7

52.4136

29.21701

13.7

5.6

80.7

0

30.416

35.65789

%EA

%EA

METHOD PM

Test No. 7
Run No. 1

Test Date(s) 1/12/95

AQD File 27A

Unit tested: No.2 Boiler

sqrt avg dp 1.048106

counter 24

sum sqrt 1.15

1.05 1.024695

1.2 1.095445

1.2 1.095445

1.25 1.118034

1.25 1.118034

1.3 1.140175

1.35 1.161895

1.25 1.118034

1.1 1.048809

0.93 0.964365

0.95 0.974679

1.08 1.03923

1.03 1.014889

1.02 1.00995

1.03 1.014889

1.04 1.019804

1.04 1.019804

1.04 1.019804

1.04 1.019804

1.04 1.019804

1.04 1.019804

1.01 1.004988

0

0

0

0

0

0

0

METHOD PM

Test No. 8

Test Date(s) 1/13/95

Run No. 1

AQD File 27A

Unit tested: Fine Crusher¹sqrt avg dp
counter0.823571
12

Nozzle diameter
Stack Diameter
Area of nozzle
Area of stack
time of run
meter coefficient

Dn 0.25 inches
Ds 45.49705 inches
Area n 0.000341 square feet
Area s 5.67 square feet
theta 60 minutes
gamma 0.9932 unitless

A(stack)
D(stack) 32.24244

I 0 inches
w 0 inches
De #DIV/0!
As 0 sq ft

0.65
0.7
0.7
0.8

volume of water in impingers
volume of water in silica gel

Vwc 1 ml
Vwsg 15 grams
Vwc sid 0.04707 scf
Vwsg sid 0.70725 scf

front mass 2.16E-02 grams
back mass 0.0017 grams
total mass 0.0233 grams

0.7
0.58
0.75
0.75

Moisture content of gas
vol of gas as measured by dry gas meter

Bws 0.013576 fraction
Vim 54.72 def

front C 0.00608086 gr/dscf
front C 8.6869E-07 lb/dscf
front C 0.79794895 lb/hr

0.74
0.860233
0.7
0.83666

pilot tube coefficient
pilot tube constant

Cp 0.84
Kp 85.49

*const
back C 6.8369E-08 lb/dscf
back C 0.06280154 lb/hr

0.6
0.774597
0.5
0.707107

Stack temperature (F +460)
Meter temperature (F +460)
barometric pressure

Tm 511.1 R
Ts 529 R
Pg 29.02 in Hg
Pg -0.25 in H2O

total C 0.00655945 gr/dscf
total C 9.3706E-07 lb/dscf
total C 0.86075049 lb/hr

0
0
0
0

static pressure
Absolute stack gas pressure

Pg 29.00161765 in Hg
Ps 2.56 in Hg

total C 0.01502381 grams/dscm
total C 425.427039 micrograms/dscf
total C 15.0238139 mg/dscm

0
0
0
0

ave press diff across orifice meter
ave of square root delta p's

delta H 0.823571 inch
delta p 47.15414 ft/s

Uncorrected
at 7%O2
at 12%CO2

0
0
0
0

Stack gas velocity
Stack gas volumetric flow rate

Vs 16041.84 acfm
Qa 15309.35 dscfm

#VALUE!
#VALUE!

0
0
0
0

Stack gas dry volumetric flow rate
Wet molecular weight

Vnsd 54.80934
Ms 28.69363

0.03
20.9
79.07
0
28.8408
-81896.55

0
0
0
0
0
0

Dry molecular weight
CONCENTRATION FROM F FACTOR For Total

%EA

0

0

F-factor
C

dscf/nmbtu
9E-07 lb/dscf

Front Only
8.69E-07 lb/dscf

0

Fo
E*

0
#DIV/0!

Back Only
#DIV/0!

0

I intermediate values
I raw

99.306 %
97.985 %

6.84E-08 lb/dscf
#DIV/0!

0
0

METHOD PM

Test No. 9

Test Date(s) 1/13/95

Run No. 1

AQD File 27A

Nozzle diameter

Dn

inches

A(stack)

Unit tested: Dry Cobber #

I

O inches

sqrt avg dp
counter0.96543
24

Stack Diameter

Ds

inches

A(stack)

20.46

w

O inches

0.91

0.953939

Area of nozzle

Area n

square feet

D(stack)

61.24761

De

O inches

0.9

0.948683

Area of stack

Area s

square feet

D(stack)

61.24761

As

O sq ft

0.92

0.959166

time of run

theta

minutes

D(stack)

61.24761

As

O sq ft

0.91

0.953939

meter coefficient

gamma

unitless

D(stack)

61.24761

As

O sq ft

0.95

0.974679

volume of water in impingers

Vwc

ml

D(stack)

61.24761

As

O sq ft

0.94

0.969536

volume of water in silica gel

Vwsg

grams

D(stack)

61.24761

As

O sq ft

0.93

0.964365

volume of water in silica gel

Vwsg

grams

D(stack)

61.24761

As

O sq ft

0.99

0.994987

volume of water in silica gel

Vwsg

grams

D(stack)

61.24761

As

O sq ft

0.99

0.994987

Moisture content of gas

Bws

fraction

D(stack)

61.24761

As

O sq ft

0.94

0.969536

vol of gas as measured by dry gas meter

Vm

def

D(stack)

61.24761

As

O sq ft

0.97

0.984886

pilot tube coefficient

Cp

*const

D(stack)

61.24761

As

O sq ft

0.88

0.938083

pilot tube constant

Kp

*const

D(stack)

61.24761

As

O sq ft

0.95

0.974679

Stack temperature (F +460)

Ts

R

D(stack)

61.24761

As

O sq ft

0.98

0.989949

Meter temperature (F +460)

Tm

R

D(stack)

61.24761

As

O sq ft

0.97

0.984886

barometric pressure

Pb

in Hg

D(stack)

61.24761

As

O sq ft

0.99

0.994987

static pressure

Pg

in H2O

D(stack)

61.24761

As

O sq ft

0.99

0.994987

Absolute stack gas pressure

Ps

in Hg

D(stack)

61.24761

As

O sq ft

0.97

0.984886

ave press diff across orifice meter

delta H

inches

D(stack)

61.24761

As

O sq ft

0.99

0.994987

ave of square root delta p's

delta H

inches

D(stack)

61.24761

As

O sq ft

0.99

0.994987

Stack gas velocity

Vs

ft/s

D(stack)

61.24761

As

O sq ft

0.92

0.959166

Stack gas volumetric flow rate

Qa

acfm

D(stack)

61.24761

As

O sq ft

0.83

0.911043

Stack gas dry volumetric flow rate

Qsd

dscfm

D(stack)

61.24761

As

O sq ft

0.73

0.8544

Wet molecular weight

Mws

at 12%CO2

D(stack)

61.24761

As

O sq ft

0.8

0.894427

Dry molecular weight

Mds

at 12%CO2

D(stack)

61.24761

As

O sq ft

0.8

0.894427

CONCENTRATION FROM F FACTOR For Total

F-factor

Front Only

D(stack)

61.24761

As

O sq ft

0.99

0.994987

C

1E-06

Back Only

D(stack)

61.24761

As

O sq ft

0.92

0.959166

Fo

0

Back Only

D(stack)

61.24761

As

O sq ft

0.83

0.911043

E*

#DIV/OI

Back Only

D(stack)

61.24761

As

O sq ft

0.73

0.8544

I intermediate values

#DIV/OI

Back Only

D(stack)

61.24761

As

O sq ft

0.99

0.994987

I raw

#DIV/OI

Back Only

D(stack)

61.24761

As

O sq ft

0.99

0.994987

I raw

#DIV/OI

Back Only

D(stack)

61.24761

As

O sq ft

0.99

0.994987

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APPENDICES:

- A - Volumetric Flow Rate Determinations
- B - Location of Test Ports
- C - Field Data Sheets
- D - Interpoll Laboratories Analytical Data
- E - Required Data for Combustion Sources
- F - Operational Data
- G - Procedures
- H - Calculation Equations
- I - Sampling Train Calibration Data
- J - Test Plan

ACFM	actual cubic feet per minute
cc (ml)	cubic centimeter (milliliter)
DSCFM	dry standard cubic foot of dry gas per minute
DSML	dry standard milliliter
DEG-F (°F)	degrees Fahrenheit
DIA.	diameter
FP	finished product for plant
FT/SEC	feet per second
g	gram
GPM	gallons per minute
GR/ACF	grains per actual cubic foot
GR/DSCF	grains per dry standard cubic foot
g/dscm	grams per dry standard cubic meter
HP	horsepower
HRS	hours
IN.	inches
IN.HG.	inches of mercury
IN.WC.	inches of water
LB	pound
LB/DSCF	pounds per dry standard cubic foot
LB/HR	pounds per hour
LB/10 ⁶ BTU	pounds per million British Thermal Units heat input
LB/MMBTU	pounds per million British Thermal Units heat input
LTPD	long tons per day
MW	megawatt
mg/Nm ³	milligrams per dry standard cubic meter
ug/Nm ³	micrograms per dry standard cubic meter
microns (um)	micrometer
MIN.	minutes
ng	nanograms
ohm-cm	ohm-centimeter
PM	particulate matter
PPH	pounds per hour
PPM	parts per million
ppmC	parts per million carbon
ppm,d	parts per million, dry
ppm,w	parts per million, wet
ppt	parts per trillion
PSI	pounds per square inch
SQ.FT.	square feet
TPD	tons per day
ug	micrograms
v/v	percent by volume
w/w	percent by weight
<	≤ (when following a number)

Standard conditions are defined as 68°F (20°C) and 29.92 IN. of mercury pressure.

g:\stackwpl\misc\abbrev.fm

Certifications Required For Performance Test Reports

Note: All performance test reports must contain a certification by the responsible parties that the test results have been reported accurately, that the field data is a true representation of the sampling procedures, and that the process data is a true indicator of the operating parameters of the emissions unit at the time of the performance test. (Ref. Minn. Rules pt. 7017.2040). Performance test results will not be accepted without certification of the report.

1. Certification of sampling procedures by the team leader of the personnel conducting the sampling procedures:

"I certify under penalty of law that the sampling procedures were performed in accordance with the approved test plan and that the data presented in this test report are, to the best of my knowledge and belief, true, accurate, and complete. All exceptions are listed and explained below."

Signature: Duane Van Hoever
Title: Field Engineer

Printed Name of Person Signing: Duane Van Hoever
Date: 6/13/95

2. Certification of analytical procedures by the person responsible for the laboratory analysis of field samples:

"I certify under penalty of law that the analytical procedures were performed in accordance with the requirements of the test methods and that the data presented for use in the test report were, to the best of my knowledge and belief, true, accurate, and complete. All exceptions are listed and explained below."

Signature: David Schneider
Title: QA Officer

Printed Name of Person Signing: David Schneider
Date: 2/16/95

3. Certification of test report by the senior staff person at the testing company who is responsible for compiling and checking the test report:

"I certify under penalty of law that this test report and all attachments were prepared under my direction or supervision in accordance with a system designed to assure that qualified personnel properly gathered and evaluated the test information submitted. Based on my inquiry of the person or persons who performed sampling and analysis relating to the performance test, the information submitted in this test report is, to the best of my knowledge and belief, true, accurate, and complete. All exceptions are listed and explained below."

Signature: Daniel J. Desper
Title: Mgr. Stationary Source

Printed Name of Person Signing: Daniel J. Desper
Date: Feb 16, 1995

4. Certification of test report by owner or operator of the emission facility:

"I certify under penalty of law that the information submitted in this test report accurately reflects the operating conditions at the emission facility during this performance test and describes the date and nature of all operational and maintenance activities that were performed on process and control equipment during the month prior to the performance test. Based on my inquiry of the person or persons who performed the operational and maintenance activities, the information submitted in this test report is, to the best of my knowledge and belief, true, accurate, and complete. All exceptions are listed and explained below."

Signature: _____
Title: _____

Printed Name of Person Signing: _____
Date: _____

Certifications Required For Performance Test Reports

Note: All performance test reports must contain a certification by the responsible parties that the test results have been reported accurately, that the field data is a true representation of the sampling procedures, and that the process data is a true indicator of the operating parameters of the emissions unit at the time of the performance test. (Ref. Minn. Rules pt. 7017.2040). Performance test results will not be accepted without certification of the report.

1. Certification of sampling procedures by the team leader of the personnel conducting the sampling procedures:

"I certify under penalty of law that the sampling procedures were performed in accordance with the approved test plan and that the data presented in this test report are, to the best of my knowledge and belief, true, accurate, and complete. All exceptions are listed and explained below."

Signature: Gary Abue Printed Name of Person Signing: GARY ABUE
Title: FIELD TECH Date: 1-13-95

2. Certification of analytical procedures by the person responsible for the laboratory analysis of field samples:

"I certify under penalty of law that the analytical procedures were performed in accordance with the requirements of the test methods and that the data presented for use in the test report were, to the best of my knowledge and belief, true, accurate, and complete. All exceptions are listed and explained below."

Signature: David J. Schneider Printed Name of Person Signing: David Schneider
Title: QA Officer Date: 2/16/95

3. Certification of test report by the senior staff person at the testing company who is responsible for compiling and checking the test report:

"I certify under penalty of law that this test report and all attachments were prepared under my direction or supervision in accordance with a system designed to assure that qualified personnel properly gathered and evaluated the test information submitted. Based on my inquiry of the person or persons who performed sampling and analysis relating to the performance test, the information submitted in this test report is, to the best of my knowledge and belief, true, accurate, and complete. All exceptions are listed and explained below."

Signature: Daniel J. Despen Printed Name of Person Signing: Daniel J. Despen
Title: Mgr. Stationary Source Date: Feb 16, 1995

4. Certification of test report by owner or operator of the emission facility:

"I certify under penalty of law that the information submitted in this test report accurately reflects the operating conditions at the emission facility during this performance test and describes the date and nature of all operational and maintenance activities that were performed on process and control equipment during the month prior to the performance test. Based on my inquiry of the person or persons who performed the operational and maintenance activities, the information submitted in this test report is, to the best of my knowledge and belief, true, accurate, and complete. All exceptions are listed and explained below."

Signature: _____ Printed Name of Person Signing: _____
Title: _____ Date: _____

Certifications Required For Performance Test Reports

Note: All performance test reports must contain a certification by the responsible parties that the test results have been reported accurately, that the field data is a true representation of the sampling procedures, and that the process data is a true indicator of the operating parameters of the emissions unit at the time of the performance test. (Ref. Minn. Rules pt. 7017.2040). Performance test results will not be accepted without certification of the report.

1. Certification of sampling procedures by the team leader of the personnel conducting the sampling procedures:

"I certify under penalty of law that the sampling procedures were performed in accordance with the approved test plan and that the data presented in this test report are, to the best of my knowledge and belief, true, accurate, and complete. All exceptions are listed and explained below."

Signature: _____

Jeff Scripte
Field Engineer

Printed Name of Person Signing: _____

Jeff Scripte

Title: _____

Date: _____

1/12/95

2. Certification of analytical procedures by the person responsible for the laboratory analysis of field samples:

"I certify under penalty of law that the analytical procedures were performed in accordance with the requirements of the test methods and that the data presented for use in the test report were, to the best of my knowledge and belief, true, accurate, and complete. All exceptions are listed and explained below."

Signature: _____

David J. Schneider

Printed Name of Person Signing: _____

David Schneider

Title: _____

QA Officer

Date: _____

2/16/95

3. Certification of test report by the senior staff person at the testing company who is responsible for compiling and checking the test report:

"I certify under penalty of law that this test report and all attachments were prepared under my direction or supervision in accordance with a system designed to assure that qualified personnel properly gathered and evaluated the test information submitted. Based on my inquiry of the person or persons who performed sampling and analysis relating to the performance test, the information submitted in this test report is, to the best of my knowledge and belief, true, accurate, and complete. All exceptions are listed and explained below."

Signature: _____

Daniel J. Dessen
Mgr. Stationary Source

Printed Name of Person Signing: _____

Daniel J. Dessen

Title: _____

Date: _____

Feb 16, 1995

4. Certification of test report by owner or operator of the emission facility:

"I certify under penalty of law that the information submitted in this test report accurately reflects the operating conditions at the emission facility during this performance test and describes the date and nature of all operational and maintenance activities that were performed on process and control equipment during the month prior to the performance test. Based on my inquiry of the person or persons who performed the operational and maintenance activities, the information submitted in this test report is, to the best of my knowledge and belief, true, accurate, and complete. All exceptions are listed and explained below."

Signature: _____

Printed Name of Person Signing: _____

Title: _____

Date: _____

Certifications Required For Performance Test Reports

Note: All performance test reports must contain a certification by the responsible parties that the test results have been reported accurately, that the field data is a true representation of the sampling procedures, and that the process data is a true indicator of the operating parameters of the emissions unit at the time of the performance test. (Ref. Minn. Rules pt. 7017.2040). Performance test results will not be accepted without certification of the report.

1. Certification of sampling procedures by the team leader of the personnel conducting the sampling procedures:

"I certify under penalty of law that the sampling procedures were performed in accordance with the approved test plan and that the data presented in this test report are, to the best of my knowledge and belief, true, accurate, and complete. All exceptions are listed and explained below."

Signature: E. Troublidar
Title: FIELD ENG

Printed Name of Person Signing: E. TROUBLIDAR
Date: 1-10-95

2. Certification of analytical procedures by the person responsible for the laboratory analysis of field samples:

"I certify under penalty of law that the analytical procedures were performed in accordance with the requirements of the test methods and that the data presented for use in the test report were, to the best of my knowledge and belief, true, accurate, and complete. All exceptions are listed and explained below."

Signature: David Schneider
Title: QA OFFICER

Printed Name of Person Signing: David Schneider
Date: 2/16/95

3. Certification of test report by the senior staff person at the testing company who is responsible for compiling and checking the test report:

"I certify under penalty of law that this test report and all attachments were prepared under my direction or supervision in accordance with a system designed to assure that qualified personnel properly gathered and evaluated the test information submitted. Based on my inquiry of the person or persons who performed sampling and analysis relating to the performance test, the information submitted in this test report is, to the best of my knowledge and belief, true, accurate, and complete. All exceptions are listed and explained below."

Signature: Daniel J. Dessen
Title: Mgr. Stationary Source

Printed Name of Person Signing: Daniel J. Dessen
Date: Feb 16, 1995

4. Certification of test report by owner or operator of the emission facility:

"I certify under penalty of law that the information submitted in this test report accurately reflects the operating conditions at the emission facility during this performance test and describes the date and nature of all operational and maintenance activities that were performed on process and control equipment during the month prior to the performance test. Based on my inquiry of the person or persons who performed the operational and maintenance activities, the information submitted in this test report is, to the best of my knowledge and belief, true, accurate, and complete. All exceptions are listed and explained below."

Signature: _____
Title: _____

Printed Name of Person Signing: _____
Date: _____

1 INTRODUCTION

During January 10 - 13, 1995 Interpoll Laboratories personnel conducted the following air emission tests at the Northshore Mining Facility in Silver Bay, Minnesota:

Source	Parameters	Date
Bin Storage Stack	PM	1-10-95
No. 1105 Pelletizer Waste Gas Stack	PM	1-10-95
No. 1104 Pelletizer Waste Gas Stack	PM	1-10-95
No. 1205 Waste Gas Stack	PM,SO ₂ ,NO _x	1-11-95
No. 1204 Waste Gas Stack	PM	1-11-95
Rotoclone Stack	PM	1-12-95
No. 2 Boiler Stack	PM,SO ₂	1-12-95
Fine Crusher Stack	PM	1-13-95
Dry Cobber Stack	PM	1-13-95

On-site testing was performed by Duane Van Hoever, Ed Trowbridge, Gary Hove, Jeff Scriptor, Scott Fjelsta, Todd Franceen, and Jamie Bainville. Coordination between testing activities and plant operation was provided by Dennis Wagner of Northshore Mining. The tests were witnessed by Dave Vaaler of the Minnesota Pollution Control Agency.

Particulate evaluations were performed in accordance with EPA Methods 1 - 5, CFR Title 40, Part 60, Appendix A (revised July 1, 1993). A preliminary determination of the gas linear velocity profile was made at each test site before the first particulate determination to allow selection of the appropriate nozzle diameter required for isokinetic sample withdrawal. An Interpoll Labs sampling train which meets or exceeds specifications in the above-cited reference was used to extract particulate samples by means of a heated glass-lined probe. Wet catch samples were collected in the back half of the Method 5 sampling train and analyzed as per Minnesota Rules, Part 7011.0725. Sulfur dioxide samples were collected in accordance with EPA Method 6 using the large impinger version without the isopropanol preimpinger. The recovered samples were returned to the laboratory for sulfate analyses by the standard barium/Thorin I titration.

The oxides of nitrogen samples were collected during the particulate determinations

using an all-glass Method 7 sampling train. A heated stainless steel probe was used to extract the samples from the exhaust stream. A plug of glass-wool was used in the end of the probe to remove particulate material.

The NO_x samples were collected in volume-calibrated two-liter all-glass flasks. An aliquot of 25 cc of absorbing solution was added to each flask on-site; the flask was closed; inserted into the sampling train; and evacuated. The probe was then purged and the sample collected over a 15 second interval. The flask was then closed; the flask removed from the sampling train; shook for two minutes and then secured for transport to the laboratory.

Upon arrival at the laboratory, the NO_x samples are logged in, placed in a designated area and maintained at 72 °F for 24 hours to allow completion of the conversion of NO to NO_2 and absorption in the acidified peroxide reagent. The flasks are then shook to complete absorption; attached to a mercury manometer and the static pressure and temperature recorded. The samples are then recovered and analyzed by ion chromatography.

Testing on the Bin Storage Stack was conducted from 2 test ports oriented at 90 degrees on the stack. The test ports are located 3.3 diameters downstream and 9.1 diameters upstream of the nearest flow disturbances. A 12 point/5 minute per point traverse was used for a total of 60 minutes per run. Visible emissions determinations were attempted by Jeff Scripter, an EPA-certified observer, but were unable to be performed due to heavy snow.

Testing on the No. 1104 and No. 1105 Pelletizers was conducted from two test ports oriented at 90 degrees. The test port location meets EPA specifications. A 24-point traverse was used at each test site. Each traverse point was sampled for 2.5 minutes for a total of 60 minutes per run.

Testing on the Waste Gas Stack was conducted from two test ports oriented at 90 degrees. The test port location meets EPA specifications. A 24-point traverse was used to collect representative particulate and sulfur dioxide samples. Each point was sampled for 2.5 minutes for a total of 60 minutes per run.

Testing on the Rotoclone Stack was conducted from 2 test ports oriented at 90 degrees on the stack. The test ports are located 5.3 diameters downstream and 1.4 diameters

upstream of the nearest flow disturbances. A 20-point traverse was used to collect representative particulate samples. Each point was sampled for 3 minutes for a total sampling time of 60 minutes per run.

Testing on the No. 2 Boiler was conducted from 2 test ports oriented at 90 degrees on the stack. The test ports are located 13 diameters downstream and 0.6 diameters upstream of the nearest flow disturbances. A 24-point traverse was to collect representative particulate samples. Each point was sampled for 2.5 minutes for a total of 60 minutes per run. Visible emissions observations were attempted by Jeff Scriptor, an EPA-certified observer, but were unable to be performed due to heavy snow.

Testing on the Fine Crusher was conducted from 2 test ports oriented at 90 degrees on the stack. The test ports are located 9.5 stack diameters downstream and 9.5 diameters upstream of the nearest flow disturbances. A 12-point/5 minute per point traverse was used for a total of 60 minutes per run.

Testing on the Dry Cobber was conducted from 2 test ports oriented at 90 degrees on the stack. The test ports are located 2.7 stack diameters downstream and 0.81 diameters upstream of the nearest flow disturbances. A 24-point/2.5 minute per point traverse was used for a total of 60 minutes per run. Visible emissions observations were attempted by Jeff Scriptor, an EPA-certified observer, but were unable to be performed due to heavy snow.

The important results of the test are summarized in Section 2. Detailed results are presented in Section 3. Field data and all other supporting information are presented in the appendices.

The results of the air emission compliance tests are summarized in Tables 1 - 11. An overview of these results and their emission limits is presented below:

Please Note: Opacity observations were attempted, but were unable to be performed due to poor weather conditions.

PARAMETER	Limit	MEASURED
<u>EMISSION POINT 76</u>		
Rotoclone Stack		
Particulate GR/DSCF)	0.03	0.0069
. (LB/HR)	N/A	2.0
<u>EMISSION POINT 2</u>		
No. 2 Boiler Stack		
Particulate (LB/10 ⁶ BTU)	0.6	0.017
Sulfur Dioxide . . . (LB/10 ⁶ BTU)	2.5	0.47
*Opacity (%)	20	N/A
<u>EMISSION POINT 11</u>		
No. 2 Fine Crusher Stack		
Particulate (GR/DSCF)	0.002	0.0047
. (LB/HR)	N/A	0.62
*Opacity (%)	20	N/A
<u>EMISSION POINT 22</u>		
Dry Cobber Stack		
Particulate (GR/DSCF)	0.01	0.005
. (LB/HR)	N/A	2.8
*Opacity (%)	20	N/A

Please Note: Opacity observations were attempted, but were unable to be performed due to poor weather conditions.

No difficulties were encountered in the field or in the laboratory evaluation of the samples. On the basis of these facts and a complete review of the data and results, it is our opinion that the results reported herein are accurate and closely reflect the actual values which existed at the time the test was performed.

Table 1a. Summary of the Results of the January 10, 1995 Particulate Emission Compliance Test on the Bin Storage Stack at the Northshore Mining Facility Located in Silver Bay, Minnesota.

ITEM	Run 1	Run 2	Run 3
Date of test	01-10-95	01-10-95	01-10-95
Time runs were done (HRS)	830/ 938	958/1102	1116/1220
Process rate			
Volumetric flow actual (ACFM)	28838	29765	29753
standard (DSCFM)	28616	29522	29692
Gas temperature (DEG-F)	58	57	55
Moisture content (%V/V)	0.99	1.18	0.95
Gas composition (%V/V, dry)			
carbon dioxide	0.03	0.03	0.03
oxygen	20.90	20.90	20.90
nitrogen	79.07	79.07	79.07
Isokinetic variation (%)	99.6	100.3	99.9
Particulate concentration			
actual (GR/ACF)	.00476	.00544	.00625
standard (GR/DSCF)	.00480	.00549	.00626
Part. emission rate (LB/HR)	1.18	1.39	1.59

Note: Dry + Organic Wet Catch

Table 1b. Summary of the Results of the January 10, 1995 Particulate Emission Compliance Test on the Bin Storage Stack at the Northshore Mining Facility Located in Silver Bay, Minnesota.

ITEM	Run 1	Run 2	Run 3
Date of test	01-10-95	01-10-95	01-10-95
Time runs were done (HRS)	830/ 938	958/1102	1116/1220
Process rate			
Volumetric flow actual (ACFM)	28838	29765	29753
standard (DSCFM)	28616	29522	29692
Gas temperature (DEG-F)	58	57	55
Moisture content (%V/V)	0.99	1.18	0.95
Gas composition (%V/V, dry)			
carbon dioxide	0.03	0.03	0.03
oxygen	20.90	20.90	20.90
nitrogen	79.07	79.07	79.07
Isokinetic variation (%)	99.6	100.3	99.9
Particulate concentration actual (GR/ACF)	.00472	.00513	.00578
standard (GR/DSCF)	.00476	.00518	.00579
Part. emission rate (LB/HR)	1.17	1.31	1.47

Note: Dry Catch Only

Table 2a. Summary of the Results of the January 10, 1995 Particulate Emission Compliance Test on the No. 1105 Pelletizer Stack at the Northshore Mining Facility Located in Silver Bay, Minnesota.

ITEM	Run 1	Run 2	Run 3
Date of test	01-10-95	01-10-95	01-10-95
Time runs were done (HRS)	827/ 932	1003/1152	1226/1327
Process rate			
Volumetric flow actual (ACFM) standard (DSCFM)	93717 70316	97113 72787	93302 70134
Gas temperature (DEG-F)	128	129	128
Moisture content (%V/V)	14.79	14.86	14.68
Gas composition (%V/V, dry) carbon dioxide oxygen nitrogen	1.80 17.20 81.00	1.80 17.30 80.90	1.80 17.20 81.00
Isokinetic variation (%)	101.3	99.7	100.2
Particulate concentration actual (GR/ACF) standard (GR/DSCF)	.00768 .0102	.00803 .0107	.00859 .0114
Part. emission rate (LB/HR)	6.17	6.69	6.88

Note: Dry + Organic Wet Catch

Table 2b. Summary of the Results of the January 10, 1995 Particulate Emission Compliance Test on the No. 1105 Pelletizer Stack at the Northshore Mining Facility Located in Silver Bay, Minnesota.

ITEM	Run 1	Run 2	Run 3
Date of test	01-10-95	01-10-95	01-10-95
Time runs were done (HRS)	827/ 932	1003/1152	1226/1327
Process rate			
Volumetric flow actual (ACFM) standard (DSCFM)	93717 70316	97113 72787	93302 70134
Gas temperature (DEG-F)	128	129	128
Moisture content (%V/V)	14.79	14.86	14.68
Gas composition (%V/V, dry) carbon dioxide oxygen nitrogen	1.80 17.20 81.00	1.80 17.30 80.90	1.80 17.20 81.00
Isokinetic variation (%)	101.3	99.7	100.2
Particulate concentration actual (GR/ACF) standard (GR/DSCF)	.00687 .00917	.00749 .00999	.00773 .0103
Part. emission rate (LB/HR)	5.52	6.23	6.18

Note: Dry Catch Only

Table 3a. Summary of the Results of the January 10, 1995 Particulate Emission Compliance Test on the No. 1104 Pelletizer Stack at the Northshore Mining Facility Located in Silver Bay, Minnesota.

ITEM	Run 1	Run 2	Run 3
Date of test	01-10-95	01-10-95	01-10-95
Time runs were done (HRS)	830/ 935	1005/1155	1226/1330
Process rate			
Volumetric flow actual (ACFM) standard (DSCFM)	93129 69343	93410 69067	93219 69437
Gas temperature (DEG-F)	132	132	131
Moisture content (%V/V)	15.00	15.61	15.12
Gas composition (%V/V, dry) carbon dioxide oxygen nitrogen	1.90 17.20 80.90	1.90 17.20 80.90	1.90 17.20 80.90
Isokinetic variation (%)	99.5	100.3	100.0
Particulate concentration actual (GR/ACF) standard (GR/DSCF)	.00876 .0118	.00656 .00887	.00465 .00625
Part. emission rate (LB/HR)	6.99	5.25	3.72

Note: Dry + Organic Wet Catch

Table 3b. Summary of the Results of the January 10, 1995 Particulate Emission Compliance Test on the No. 1104 Pelletizer Stack at the Northshore Mining Facility Located in Silver Bay, Minnesota.

ITEM	Run 1	Run 2	Run 3
Date of test	01-10-95	01-10-95	01-10-95
Time runs were done (HRS)	830/ 935	1005/1155	1226/1330
Process rate			
Volumetric flow actual (ACFM) standard (DSCFM)	93129 69343	93410 69067	93219 69437
Gas temperature (DEG-F)	132	132	131
Moisture content (%V/V)	15.00	15.61	15.12
Gas composition (%V/V, dry) carbon dioxide oxygen nitrogen	1.90 17.20 80.90	1.90 17.20 80.90	1.90 17.20 80.90
Isokinetic variation (%)	99.5	100.3	100.0
Particulate concentration actual (GR/ACF) standard (GR/DSCF)	.00847 .0114	.00629 .00851	.00414 .00556
Part. emission rate (LB/HR)	6.76	5.04	3.31

Note: Dry Catch Only

Table 4a. Summary of the Results of the January 11, 1995 Particulate Emission Compliance Test on the No. 1205 Waste Gas Stack at the Northshore Mining Facility Located in Silver Bay, Minnesota.

ITEM	Run 1	Run 2	Run 3
Date of test	01-11-95	01-11-95	01-11-95
Time runs were done (HRS)	840/ 940	1022/1125	1153/1253
Process rate			
Volumetric flow actual (ACFM)	88656	91102	89277
standard (DSCFM)	65952	63717	61936
Gas temperature (DEG-F)	138	140	139
Moisture content (%V/V)	13.18	18.07	18.92
Gas composition (%V/V, dry)			
carbon dioxide	2.10	2.00	2.00
oxygen	16.80	16.80	17.00
nitrogen	81.10	81.20	81.00
Isokinetic variation (%)	97.4	102.7	101.7
Particulate concentration			
actual (GR/ACF)	.00741	.00648	.00648
standard (GR/DSCF)	.00997	.00926	.00935
Part. emission rate (LB/HR)	5.64	5.06	4.96

Note: Dry + Organic Wet Catch

Table 4b. Summary of the Results of the January 11, 1995 Particulate Emission Compliance Test on the No. 1205 Waste Gas Stack at the Northshore Mining Facility Located in Silver Bay, Minnesota.

ITEM	Run 1	Run 2	Run 3
Date of test	01-11-95	01-11-95	01-11-95
Time runs were done (HRS)	840/ 940	1022/1125	1153/1253
Process rate			
Volumetric flow actual (ACFM)	88656	91102	89277
standard (DSCFM)	65952	63717	61936
Gas temperature (DEG-F)	138	140	139
Moisture content (%V/V)	13.18	18.07	18.92
Gas composition (%V/V.dry)			
carbon dioxide	2.10	2.00	2.00
oxygen	16.80	16.80	17.00
nitrogen	81.10	81.20	81.00
Isokinetic variation (%)	97.4	102.7	101.7
Particulate concentration			
actual (GR/ACF)	.00642	.00546	.00537
standard (GR/DSCF)	.00863	.00781	.00774
Part. emission rate (LB/HR)	4.88	4.27	4.11

Note: Dry Catch Only

Table 5a. Summary of the Results of the January 11, 1995 Particulate Emission Compliance Test on the No. 1204 Waste Gas Stack at the Northshore Mining Facility Located in Silver Bay, Minnesota.

ITEM	Run 1	Run 2	Run 3
Date of test	01-11-95	01-11-95	01-11-95
Time runs were done (HRS)	840/ 942	1022/1126	1153/1257
Process rate			
Volumetric flow actual (ACFM)	91099	89531	90737
standard (DSCFM)	63727	62512	63698
Gas temperature (DEG-F)	140	139	139
Moisture content (%V/V)	18.06	18.37	17.98
Gas composition (%V/V, dry)			
carbon dioxide	2.00	2.00	2.10
oxygen	16.80	16.90	16.80
nitrogen	81.20	81.10	81.10
Isokinetic variation (%)	99.8	100.1	99.9
Particulate concentration			
actual (GR/ACF)	.005553	.004320	.005407
standard (GR/DSCF)	.007942	.006190	.007705
Part. emission rate (LB/HR)	4.34	3.32	4.21

Note: Dry + Organic Wet Catch

Table 5b. Summary of the Results of the January 11, 1995 Particulate Emission Compliance Test on the No. 1204 Waste Gas Stack at the Northshore Mining Facility Located in Silver Bay, Minnesota.

ITEM	Run 1	Run 2	Run 3
Date of test	01-11-95	01-11-95	01-11-95
Time runs were done (HRS)	840/ 942	1022/1126	1153/1257
Process rate			
Volumetric flow actual (ACFM)	91099	89531	90737
standard (DSCFM)	63727	62512	63698
Gas temperature (DEG-F)	140	139	139
Moisture content (%V/V)	18.06	18.37	17.98
Gas composition (%V/V, dry)			
carbon dioxide	2.00	2.00	2.10
oxygen	16.80	16.90	16.80
nitrogen	81.20	81.10	81.10
Isokinetic variation (%)	99.8	100.1	99.9
Particulate concentration			
actual (GR/ACF)	.005345	.004249	.005012
standard (GR/DSCF)	.007644	.006089	.007143
Part. emission rate (LB/HR)	4.18	3.26	3.90

Note: Dry Catch Only

Table 6a. Summary of the Results of the January 12, 1995 Particulate Emission Compliance Test on the Rotocclone Stack at the Northshore Mining Stack Located in Silver Bay, Minnesota.

ITEM	Run 1	Run 2	Run 3
Date of test	01-12-95	01-12-95	01-12-95
Time runs were done (HRS)	825/ 926	1005/1107	1136/1322
Process rate			
Volumetric flow actual (ACFM)	42164	42388	42523
standard (DSCFM)	33820	33708	33616
Gas temperature (DEG-F)	137	138	138
Moisture content (%V/V)	6.11	6.66	7.26
Gas composition (%V/V, dry)			
carbon dioxide	0.00	0.00	0.00
oxygen	20.90	20.90	20.90
nitrogen	79.10	79.10	79.10
Isokinetic variation (%)	92.9	100.8	101.2
Particulate concentration			
actual (GR/ACF)	.00628	.00535	.00492
standard (GR/DSCF)	.00783	.00673	.00622
Part. emission rate (LB/HR)	2.27	1.94	1.79

Note: Dry + Organic Wet Catch

Table 6b. Summary of the Results of the January 12, 1995 Particulate Emission Compliance Test on the Rotoclone Stack at the Northshore Mining Stack Located in Silver Bay, Minnesota.

ITEM	Run 1	Run 2	Run 3
Date of test	01-12-95	01-12-95	01-12-95
Time runs were done (HRS)	825/ 926	1005/1107	1136/1322
Process rate			
Volumetric flow actual (ACFM)	42164	42388	42523
standard (DSCFM)	33820	33708	33616
Gas temperature (DEG-F)	137	138	138
Moisture content (%V/V)	6.11	6.66	7.26
Gas composition (%V/V, dry)			
carbon dioxide	0.00	0.00	0.00
oxygen	20.90	20.90	20.90
nitrogen	79.10	79.10	79.10
Isokinetic variation (%)	92.9	100.8	101.2
Particulate concentration			
actual (GR/ACF)	.00608	.00510	.00470
standard (GR/DSCF)	.00758	.00641	.00595
Part. emission rate (LB/HR)	2.20	1.85	1.71

Note: Dry Catch Only

Table 7a. Summary of the Results of the January 12, 1995 Particulate Emission Compliance Test on the No. 2 Boiler Stack at the Northshore Mining Facility Located in Silver Bay, Minnesota.

ITEM	Run 1	Run 2	Run 3
Date of test	01-12-95	01-12-95	01-12-95
Time runs were done (HRS)	917/1017	1047/1147	1217/1322
Steam flow (KLB/HR)			
Volumetric flow actual (ACFM)	283059	312014	310072
standard (DSCFM)	171211	182659	179781
Gas temperature (DEG-F)	301	313	321
Moisture content (%V/V)	9.67	11.18	11.09
Gas composition (%V/V, dry)			
carbon dioxide	13.70	13.80	13.50
oxygen	5.60	5.50	5.80
nitrogen	80.70	80.70	80.70
Isokinetic variation (%)	101.2	103.7	105.0
Particulate concentration			
actual (GR/ACF)	.00609	.00470	.00501
standard (GR/DSCF)	.0101	.00803	.00865
Part. emission rate (LB/HR)	14.78	12.57	13.33
Emission factor (LB/MMBTU)	0.019	0.015	0.017

Note: Dry + Organic Wet Catch

Table 7b. Summary of the Results of the January 12, 1995 Particulate Emission Compliance Test on the No. 2 Boiler Stack at the Northshore Mining Facility Located in Silver Bay, Minnesota.

ITEM	Run 1	Run 2	Run 3
Date of test	01-12-95	01-12-95	01-12-95
Time runs were done (HRS)	917/1017	1047/1147	1217/1322
Steam flow (KLB/HR)			
Volumetric flow actual (ACFM)	283059	312014	310072
standard (DSCFM)	171211	182659	179781
Gas temperature (DEG-F)	301	313	321
Moisture content (%V/V)	9.67	11.18	11.09
Gas composition (%V/V, dry)			
carbon dioxide	13.70	13.80	13.50
oxygen	5.60	5.50	5.80
nitrogen	80.70	80.70	80.70
Isokinetic variation (%)	101.2	103.7	105.0
Particulate concentration			
actual (GR/ACF)	.00591	.00437	.00479
standard (GR/DSCF)	.00978	.00746	.00827
Part. emission rate (LB/HR)	14.35	11.68	12.74
Emission factor (LB/MMBTU)	0.019	0.014	0.016

Note: Dry Catch Only

Table 8a. Summary of the Results of the January 13, 1995 Particulate Emission Compliance Test on the Fine Crusher Stack at the Northshore Mining Facility Located in Silver Bay, Minnesota.

ITEM	Run 1	Run 2	Run 3
Date of test	01-13-95	01-13-95	01-13-95
Time runs were done (HRS)	810/ 917	1000/1105	1124/1230
Process rate			
Volumetric flow actual (ACFM)	16053	16039	16203
standard (DSCFM)	15313	15354	15512
Gas temperature (DEG-F)	69	68	67
Moisture content (%V/V)	1.36	1.27	1.42
Gas composition (%V/V, dry)			
carbon dioxide	0.03	0.03	0.03
oxygen	20.90	20.90	20.90
nitrogen	79.07	79.07	79.07
Isokinetic variation (%)	99.3	99.3	99.5
Particulate concentration			
actual (GR/ACF)	.00626	.00465	.00250
standard (GR/DSCF)	.00656	.00486	.00261
part. emission rate (LB/HR)	0.861	0.639	0.347

Note: Dry + Organic Wet Catch

Table 8b. Summary of the Results of the January 13, 1995 Particulate Emission Compliance Test on the Fine Crusher Stack at the Northshore Mining Facility Located in Silver Bay, Minnesota.

ITEM	Run 1	Run 2	Run 3
Date of test	01-13-95	01-13-95	01-13-95
Time runs were done (HRS)	810/ 917	1000/1105	1124/1230
Process rate			
Volumetric flow actual (ACFM)	16053	16039	16203
standard (DSCFM)	15313	15354	15512
Gas temperature (DEG-F)	69	68	67
Moisture content (%V/V)	1.36	1.27	1.42
Gas composition (%V/V, dry)			
carbon dioxide	0.03	0.03	0.03
oxygen	20.90	20.90	20.90
nitrogen	79.07	79.07	79.07
Isokinetic variation (%)	99.3	99.3	99.5
Particulate concentration			
actual (GR/ACF)	.00580	.00417	.00215
standard (GR/DSCF)	.00608	.00435	.00225
Part. emission rate (LB/HR)	0.798	0.573	0.299

Note: Dry Catch Only

Table 9a. Summary of the Results of the January 13, 1995 Particulate Emission Compliance Test on the Dry Cobber Stack at the Northshore Mining Facility Located in Silver Bay, Minnesota.

ITEM	Run 1	Run 2	Run 3
Date of test	01-13-95	01-13-95	01-13-95
Time runs were done (HRS)	820/ 921	1000/1105	1124/1226
Process rate			
Volumetric flow actual (ACFM)	67972	68148	67852
standard (DSCFM)	64878	65040	65558
Gas temperature (DEG-F)	71	68	67
Moisture content (%V/V)	0.83	1.48	0.27
Gas composition (%V/V, dry)			
carbon dioxide	0.03	0.03	0.03
oxygen	20.90	20.90	20.90
nitrogen	79.07	79.07	79.07
Isokinetic variation (%)	98.9	100.1	99.3
Particulate concentration			
actual (GR/ACF)	.00659	.00495	.00272
standard (GR/DSCF)	.00690	.00519	.00282
Part. emission rate (LB/HR)	3.84	2.89	1.59

Note: Dry + Organic Wet Catch

Table 9b. Summary of the Results of the January 13, 1995 Particulate Emission Compliance Test on the Dry Cobber Stack at the Northshore Mining Facility Located in Silver Bay, Minnesota.

ITEM	Run 1	Run 2	Run 3
Date of test	01-13-95	01-13-95	01-13-95
Time runs were done (HRS)	820/ 921	1000/1105	1124/1226
Process rate			
Volumetric flow actual (ACFM)	67972	68148	67852
standard (DSCFM)	64878	65040	65558
Gas temperature (DEG-F)	71	68	67
Moisture content (%V/V)	0.83	1.48	0.27
Gas composition (%V/V.dry)			
carbon dioxide	0.03	0.03	0.03
oxygen	20.90	20.90	20.90
nitrogen	79.07	79.07	79.07
Isokinetic variation (%)	98.9	100.1	99.3
Particulate concentration			
actual (GR/ACF)	.00637	.00465	.00272
standard (GR/DSCF)	.00667	.00488	.00282
part. emission rate (LB/HR)	3.71	2.72	1.59

Note: Dry Catch Only

Table 10. Summary of the Results of the January 11 & 12, 1995 Sulfur Dioxide Emission Compliance Tests at the Northshore Mining Facility in Silver Bay, Minnesota.

Test/Run	Date	Time (HRS)	Concentration (ppm,d)	Emission Rate (LB/HR)	Emission Factor (LB/10 ⁶ BTU)
(No. 1205 Waste Gas Stack)					
4/1	1-11-95	0840-0940	1	0.77	N/A
4/2	1-11-95	1022-1125	1	0.59	N/A
4/3	1-11-95	1153-1253	1	0.89	N/A
Avg			1	0.75	N/A
(No. 2 Boiler Stack)					
7/1	1-12-95	0917-1017	216	368	0.479
7/2	1-12-95	1047-1147	211	384	0.465
7/3	1-12-95	1217-1317	207	371	0.465
Avg			211	374	0.470

Table 11. Summary of the Results of the January 11, 1995 **Oxides of Nitrogen** Emission Compliance Tests at the Northshore Mining Facility in Silver Bay, Minnesota.

Test/Run	Date	Time (HRS)	Concentration (ppm,d)	Emission Rate (LB/HR)
(No. 1205 Waste Gas Stack)				
4/1	1-11-95	0840-0940	123	58
4/2	1-11-95	1022-1125	112	51
4/3	1-11-95	1153-1253	120	53
Avg			118	54

3 RESULTS

The results of all field and laboratory evaluations are presented in this section. Gas composition (Orsat and moisture) are presented first followed by the computer printout of the particulate, sulfur dioxide, oxides of nitrogen, and opacity observations. Preliminary measurements including test port locations are given in the appendices.

The results have been calculated on a personal computer using programs written in Extended BASIC specifically for source testing calculations. EPA-published equations have been used as the basis of the calculation techniques in these programs. The particulate emission rate has been calculated using the product of the concentration times flow method.

3.1 Results of Orsat & Moisture Analysis

Test No. 1
Bin Storage Stack

Results of Orsat & Moisture Analyses-----Methods 3 & 4(%v/v)

Date of run	Run 1 01-10-95	Run 2 01-10-95	Run 3 01-10-95
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Dry basis (orsat)

carbon dioxide.....	0.03	0.03	0.03
oxygen.....	20.90	20.90	20.90
nitrogen.....	79.07	79.07	79.07

Wet basis (orsat)

carbon dioxide.....	0.03	0.03	0.03
oxygen.....	20.69	20.65	20.70
nitrogen.....	78.29	78.13	78.32
water vapor.....	0.99	1.18	0.95

Dry molecular weight.....	28.84	28.84	28.84
Wet molecular weight.....	28.73	28.71	28.74
Specific gravity.....	0.993	0.992	0.993
Water mass flow.....(LB/HR)	799	992	797

Test No. 2
No. 1105 Pelletizer Stack

Results of Orsat & Moisture Analyses-----Methods 3 & 4(%v/v)

Date of run	Run 1 01-10-95	Run 2 01-10-95	Run 3 01-10-95
Dry basis (orsat)			
carbon dioxide.....	1.80	1.80	1.80
oxygen.....	17.20	17.30	17.20
nitrogen.....	81.00	80.90	81.00
Wet basis (orsat)			
carbon dioxide.....	1.53	1.53	1.54
oxygen.....	14.66	14.73	14.68
nitrogen.....	69.02	68.88	69.11
water vapor.....	14.79*	14.86*	14.68*
Dry molecular weight.....	28.98	28.98	28.98
Wet molecular weight.....	27.35	27.35	27.36
Specific gravity.....	0.945	0.945	0.945
Water mass flow.....(LB/HR)	34369	38207	36742

* Free or condensed water in the gas stream.

FO	2.056	2.000	2.056
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Test No. 3
No. 1104 Pelletizer Stack

Results of Orsat & Moisture Analyses-----Methods 3 & 4(%v/v)

Date of run	Run 1 01-10-95	Run 2 01-10-95	Run 3 01-10-95
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Dry basis (orsat)

carbon dioxide.....	1.90	1.90	1.90
oxygen.....	17.20	17.20	17.20
nitrogen.....	80.90	80.90	80.90

Wet basis (orsat)

carbon dioxide.....	1.61	1.60	1.61
oxygen.....	14.62	14.52	14.60
nitrogen.....	68.76	68.27	68.67
water vapor.....	15.00	15.61	15.12

Dry molecular weight.....	28.99	28.99	28.99
Wet molecular weight.....	27.34	27.28	27.33
Specific gravity.....	0.944	0.942	0.944
Water mass flow.....(LB/HR)	34337	35837	34684

FO	1.947	1.947	1.947
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Test No. 5
No. 1204 Waste Gas Stack

Results of Orsat & Moisture Analyses-----Methods 3 & 4(%v/v)

Date of run	Run 1 01-11-95	Run 2 01-11-95	Run 3 01-11-95
Dry basis (orsat)			
carbon dioxide.....	2.00	2.00	2.10
oxygen.....	16.80	16.90	16.80
nitrogen.....	81.20	81.10	81.10
Wet basis (orsat)			
carbon dioxide.....	1.64	1.63	1.72
oxygen.....	13.77	13.79	13.78
nitrogen.....	66.53	66.20	66.52
water vapor.....	18.06	18.37	17.98
Dry molecular weight.....	28.99	29.00	29.01
Wet molecular weight.....	27.01	26.98	27.03
Specific gravity.....	0.933	0.932	0.934
Water mass flow.....(LB/HR)	39404	39473	38819
FO	2.050	2.000	1.952

Test No. 4
No. 1205 Waste Gas Stack

Results of Orsat & Moisture Analyses-----Methods 3 & 4(%v/v)

Date of run	Run 1 01-11-95	Run 2 01-11-95	Run 3 01-11-95
Dry basis (orsat)			
carbon dioxide.....	2.10	2.00	2.00
oxygen.....	16.80	16.80	17.00
nitrogen.....	81.10	81.20	81.00
Wet basis (orsat)			
carbon dioxide.....	1.82	1.64	1.62
oxygen.....	14.59	13.76	13.78
nitrogen.....	70.41	66.52	65.68
water vapor.....	13.18	18.07	18.92
Dry molecular weight.....	29.01	28.99	29.00
Wet molecular weight.....	27.56	27.01	26.92
Specific gravity.....	0.952	0.933	0.930
Water mass flow.....(LB/HR)	28087	39429	40532
FO	1.952	2.050	1.950

Test No. 6
Rotoclone Stack

Results of Orsat & Moisture Analyses-----Methods 3 & 4(%v/v)

Date of run	Run 1 01-12-95	Run 2 01-12-95	Run 3 01-12-95
Dry basis (orsat)			
carbon dioxide.....	0.00	0.00	0.00
oxygen.....	20.90	20.90	20.90
nitrogen.....	79.10	79.10	79.10
Wet basis (orsat)			
carbon dioxide.....	0.00	0.00	0.00
oxygen.....	19.62	19.51	19.38
nitrogen.....	74.26	73.83	73.35
water vapor.....	6.11	6.66	7.26
Dry molecular weight.....	28.84	28.84	28.84
Wet molecular weight.....	28.17	28.11	28.05
Specific gravity.....	0.973	0.971	0.969
Water mass flow.....(LB/HR)	6176	6747	7385

Test No. 7
No. 2 Boiler Stack

Results of Orsat & Moisture Analyses-----Methods 3 & 4(%v/v)

Date of run	Run 1 01-12-95	Run 2 01-12-95	Run 3 01-12-95
Dry basis (orsat)			
carbon dioxide.....	13.70	13.80	13.50
oxygen.....	5.60	5.50	5.80
nitrogen.....	80.70	80.70	80.70
Wet basis (orsat)			
carbon dioxide.....	12.37	12.26	12.00
oxygen.....	5.06	4.88	5.16
nitrogen.....	72.89	71.67	71.75
water vapor.....	9.67	11.18	11.09
Dry molecular weight.....	30.42	30.43	30.39
Wet molecular weight.....	29.21	29.04	29.02
Specific gravity.....	1.009	1.003	1.002
Water mass flow.....(LB/HR)	51431	64515	62885
FO	1.117	1.116	1.119

Test No. 8
Fine Crusher Stack

Results of Orsat & Moisture Analyses-----Methods 3 & 4(%v/v)

Date of run	Run 1 01-13-95	Run 2 01-13-95	Run 3 01-13-95
Dry basis (orsat)			
carbon dioxide.....	0.03	0.03	0.03
oxygen.....	20.90	20.90	20.90
nitrogen.....	79.07	79.07	79.07
Wet basis (orsat)			
carbon dioxide.....	0.03	0.03	0.03
oxygen.....	20.62	20.63	20.60
nitrogen.....	78.00	78.07	77.95
water vapor.....	1.36	1.27	1.42
Dry molecular weight.....	28.84	28.84	28.84
Wet molecular weight.....	28.69	28.70	28.69
Specific gravity.....	0.991	0.991	0.991
Water mass flow.....(LB/HR)	591	554	627

Test No. 9
Dry Cobber Stack

Results of Orsat & Moisture Analyses-----Methods 3 & 4(%v/v)

Date of run	Run 1 01-13-95	Run 2 01-13-95	Run 3 01-13-95
Dry basis (orsat)			
carbon dioxide.....	0.03	0.03	0.03
oxygen.....	20.90	20.90	20.90
nitrogen.....	79.07	79.07	79.07
Wet basis (orsat)			
carbon dioxide.....	0.03	0.03	0.03
oxygen.....	20.73	20.59	20.84
nitrogen.....	78.42	77.90	78.85
water vapor.....	0.83	1.48	0.27
Dry molecular weight.....	28.84	28.84	28.84
Wet molecular weight.....	28.75	28.68	28.81
Specific gravity.....	0.993	0.991	0.995
Water mass flow.....(LB/HR)	1515	2744	503

3.2 Results of Particulate Loading Determinations

Test No. 1
Bin Storage Stack

Results of Particulate Loading Determinations-----Method 5

	Run 1 01-10-95	Run 2 01-10-95	Run 3 01-10-95
Date of run			
Time run start/end.....(HRS)	830/ 938	958/1102	1116/1220
Static pressure.....(IN.WC)	-0.65	-0.65	-0.65
Cross sectional area (SQ.FT)	8.51	8.51	8.51
Pitot tube coefficient.....	.840	.840	.840
Water in sample gas			
condenser.....(ML)	0.0	0.0	0.0
impingers.....(GRAMS)	0.0	0.0	0.0
desiccant.....(GRAMS)	8.0	10.0	8.0
total.....(GRAMS)	8.0	10.0	8.0
Total particulate material..			
.....collected(grams)	0.0118	0.0140	0.0160
Gas meter coefficient.....	1.0004	1.0004	1.0004
Barometric pressure..(IN.HG)	29.46	29.46	29.46
Avg. orif.pres.drop..(IN.WC)	1.23	1.33	1.34
Avg. gas meter temp..(DEF-F)	60.5	64.9	66.6
Volume through gas meter....			
at meter conditions...(CF)	37.83	39.60	39.80
standard conditions.(DSCF)	37.90	39.35	39.42
Total sampling time....(MIN)	60.00	60.00	60.00
Nozzle diameter.....(IN)	.186	.186	.186
Avg.stack gas temp ..(DEG-F)	58	57	55
Volumetric flow rate.....			
actual.....(ACFM)	28838	29765	29753
dry standard.....(DSCFM)	28616	29522	29692
Isokinetic variation.....(%)	99.6	100.3	99.9
Particulate concentration...			
actual.....(GR/ACF)	0.00476	0.00544	0.00625
dry standard.....(GR/DSCF)	0.00480	0.00549	0.00626
Particle mass rate...(LB/HR)	1.178	1.389	1.594

Test No. 2
No. 1105 Pelletizer Stack

Results of Particulate Loading Determinations-----Method 5

	Run 1 01-10-95	Run 2 01-10-95	Run 3 01-10-95
Date of run			
Time run start/end.....(HRS)	827/ 932	1003/1152	1226/1327
Static pressure.....(IN.WC)	-0.22	-0.22	-0.22
Cross sectional area (SQ.FT)	27.49	27.49	27.49
Pitot tube coefficient.....	.840	.840	.840
Water in sample gas			
condenser.....(ML)	0.0	0.0	0.0
impingers.....(GRAMS)	167.0	190.0	180.0
desiccant.....(GRAMS)	24.0	19.0	22.0
total.....(GRAMS)	191.0	209.0	202.0
Total particulate material..			
.....collected(grams)	0.0343	0.0366	0.0378
Gas meter coefficient.....	1.0015	1.0015	1.0015
Barometric pressure..(IN.HG)	29.38	29.38	29.38
Avg. orif.pres.drop..(IN.WC)	2.59	2.71	2.51
Avg. gas meter temp..(DEF-F)	81.8	85.0	86.0
Volume through gas meter....			
at meter conditions...(CF)	53.60	54.92	53.31
standard conditions.(DSCF)	51.68	52.66	51.00
Total sampling time....(MIN)	60.00	60.00	60.00
Nozzle diameter.....(IN)	.247	.247	.247
Avg.stack gas temp ..(DEG-F)	128	129	128
Volumetric flow rate.....			
actual.....(ACFM)	93717	97113	93302
dry standard.....(DSCFM)	70316	72787	70134
Isokinetic variation.....(%)	101.3	99.7	100.2
Particulate concentration...			
actual.....(GR/ACF)	0.00768	0.00803	0.00859
dry standard.....(GR/DSCF)	0.01024	0.01072	0.01144
Particle mass rate...(LB/HR)	6.172	6.691	6.875

Test No. 3
No. 1104 Pelletizer Stack

Results of Particulate Loading Determinations-----Method 5

	Run 1 01-10-95	Run 2 01-10-95	Run 3 01-10-95
Date of run			
Time run start/end.....(HRS)	830/ 935	1005/1155	1226/1330
Static pressure.....(IN.WC)	-0.14	-0.14	-0.14
Cross sectional area (SQ.FT)	27.49	27.49	27.49
Pitot tube coefficient.....	.840	.840	.840
Water in sample gas			
condenser.....(ML)	0.0	0.0	0.0
impingers.....(GRAMS)	172.0	186.0	180.0
desiccant.....(GRAMS)	20.0	16.0	15.0
total.....(GRAMS)	192.0	202.0	195.0
Total particulate material..			
.....collected(grams)	0.0391	0.0296	0.0209
Gas meter coefficient.....	0.9932	0.9932	0.9932
Barometric pressure..(IN.HG)	29.38	29.38	29.38
Avg. orif.pres.drop..(IN.WC)	2.39	2.41	2.41
Avg. gas meter temp..(DEF-F)	78.4	82.2	84.1
Volume through gas meter....			
at meter conditions...(CF)	53.32	53.91	54.25
standard conditions:(DSCF)	51.28	51.49	51.63
Total sampling time....(MIN)	60.00	60.00	60.00
Nozzle diameter.....(IN)	.250	.250	.250
Avg.stack gas temp ..(DEG-F)	132	132	131
Volumetric flow rate.....			
actual.....(ACFM)	93129	93410	93219
dry standard.....(DSCFM)	69343	69067	69437
Isokinetic variation.....(%)	99.5	100.3	100.0
Particulate concentration...			
actual.....(GR/ACF)	0.00876	0.00656	0.00465
dry standard.....(GR/DSCF)	0.01176	0.00887	0.00625
Particle mass rate...(LB/HR)	6.993	5.251	3.717

Test No. 4
No. 1205 Waste Gas Stack

Results of Particulate Loading Determinations-----Method 5

	Run 1 01-11-95	Run 2 01-11-95	Run 3 01-11-95
Date of run			
Time run start/end.....(HRS)	840/ 940	1022/1125	1153/1253
Static pressure.....(IN.WC)	-0.03	-0.03	-0.03
Cross sectional area (SQ.FT)	27.88	27.88	27.88
Pitot tube coefficient.....	.840	.840	.840
Water in sample gas			
condenser.....(ML)	0.0	0.0	0.0
impingers.....(GRAMS)	127.0	202.0	209.0
desiccant.....(GRAMS)	21.0	17.0	14.0
total.....(GRAMS)	148.0	219.0	223.0
Total particulate material..			
.....collected(grams)	0.0297	0.0281	0.0273
Gas meter coefficient.....	1.0015	1.0015	1.0015
Barometric pressure..(IN.HG)	29.02	29.02	29.02
Avg. orif.pres.drop..(IN.WC)	1.99	2.12	1.97
Avg. gas meter temp..(DEF-F)	70.6	81.9	86.7
Volume through gas meter....			
at meter conditions...(CF)	47.33	49.21	47.82
standard conditions.(DSCF)	45.96	46.81	45.07
Total sampling time....(MIN)	60.00	60.00	60.00
Nozzle diameter.....(IN)	.247	.247	.247
Avg.stack gas temp ..(DEG-F)	138	140	139
Volumetric flow rate.....			
actual.....(ACFM)	88656	91102	89277
dry standard.....(DSCFM)	65952	63717	61936
Isokinetic variation.....(%)	97.4	102.7	101.7
Particulate concentration...			
actual.....(GR/ACF)	0.00741	0.00648	0.00648
dry standard.....(GR/DSCF)	0.00997	0.00926	0.00935
Particle mass rate...(LB/HR)	5.636	5.059	4.962

Test No. 5
No. 1204 Waste Gas Stack

Results of Particulate Loading Determinations-----Method 5

Date of run	Run 1 01-11-95	Run 2 01-11-95	Run 3 01-11-95
Time run start/end.....(HRS)	840/ 942	1022/1126	1153/1257
Static pressure.....(IN.WC)	0.26	0.26	0.26
Cross sectional area (SQ.FT)	27.88	27.88	27.88
Pitot tube coefficient.....	.840	.840	.840
Water in sample gas			
condenser.....(ML)	0.0	0.0	0.0
impingers.....(GRAMS)	205.0	209.0	204.0
desiccant.....(GRAMS)	13.0	10.0	13.0
total.....(GRAMS)	218.0	219.0	217.0
Total particulate material..			
.....collected(grams)	0.0240	0.0184	0.0233
Gas meter coefficient.....	0.9932	0.9932	0.9932
Barometric pressure...(IN.HG)	29.02	29.02	29.02
Avg. orif.pres.drop...(IN.WC)	1.92	1.90	1.97
Avg. gas meter temp...(DEF-F)	65.7	77.0	79.2
Volume through gas meter....			
at meter conditions...(CF)	47.98	48.22	49.24
standard conditions.(DSCF)	46.63	45.87	46.66
Total sampling time....(MIN)	60.00	60.00	60.00
Nozzle diameter.....(IN)	.250	.250	.250
Avg.stack gas temp ..(DEG-F)	140	139	139
Volumetric flow rate.....			
actual.....(ACFM)	91099	89531	90737
dry standard.....(DSCFM)	63727	62512	63698
Isokinetic variation.....(%)	99.8	100.1	99.9
Particulate concentration...			
actual.....(GR/ACF)	0.00555	0.00432	0.00541
dry standard.....(GR/DSCF)	0.00794	0.00619	0.00770
Particle mass rate...(LB/HR)	4.338	3.316	4.207

Test No. 6
Rotoclone Stack

Results of Particulate Loading Determinations-----Method 5

	Run 1	Run 2	Run 3
Date of run	01-12-95	01-12-95	01-12-95
Time run start/end.....(HRS)	825/ 926	1005/1107	1136/1322
Static pressure.....(IN.WC)	-0.82	-0.82	-0.82
Cross sectional area (SQ.FT)	11.29	11.29	11.29
Pitot tube coefficient.....	.840	.840	.840
Water in sample gas			
condenser.....(ML)	0.0	0.0	0.0
impingers.....(GRAMS)	33.0	44.0	7.0
desiccant.....(GRAMS)	10.0	7.0	49.0
total.....(GRAMS)	43.0	51.0	56.0
Total particulate material..			
.....collected(grams)	0.0158	0.0147	0.0136
Gas meter coefficient.....	0.9932	0.9932	0.9932
Barometric pressure...(IN.HG)	28.94	28.94	28.94
Avg. orif.pres.drop...(IN.WC)	0.87	1.02	1.01
Avg. gas meter temp...(DEF-F)	73.1	74.0	71.2
Volume through gas meter....			
at meter conditions...(CF)	32.67	35.40	35.23
standard conditions.(DSCF)	31.14	33.70	33.71
Total sampling time....(MIN)	60.00	60.00	60.00
Nozzle diameter.....(IN)	.185	.185	.185
Avg.stack gas temp ..(DEG-F)	137	138	138
Volumetric flow rate.....			
actual.....(ACFM)	42164	42388	42523
dry standard.....(DSCFM)	33820	33708	33616
Isokinetic variation.....(%)	92.9	100.8	101.2
Particulate concentration...			
actual.....(GR/ACF)	0.00628	0.00535	0.00492
dry standard.....(GR/DSCF)	0.00783	0.00673	0.00622
Particle mass rate...(LB/HR)	2.269	1.945	1.794

Test No. 7
No. 2 Boiler Stack

Results of Particulate Loading Determinations-----Method 5

	Run 1	Run 2	Run 3
Date of run	01-12-95	01-12-95	01-12-95
Time run start/end.....(HRS)	917/1017	1047/1147	1217/1322
Static pressure.....(IN.WC)	-0.90	-0.90	-0.90
Cross sectional area (SQ.FT)	66.00	66.00	66.00
Pitot tube coefficient.....	.840	.840	.840
Water in sample gas			
condenser.....(ML)	0.0	0.0	0.0
impingers.....(GRAMS)	104.0	136.0	137.0
desiccant.....(GRAMS)	15.0	17.0	14.0
total.....(GRAMS)	119.0	153.0	151.0
Total particulate material..			
.....collected(grams)	0.0342	0.0298	0.0320
Gas meter coefficient.....	1.0026	1.0026	1.0026
Barometric pressure..(IN.HG)	28.94	28.94	28.94
Avg. orif.pres.drop..(IN.WC)	2.62	3.20	3.14
Avg. gas meter temp..(DEF-F)	73.6	86.6	84.7
Volume through gas meter....			
at meter conditions...(CF)	54.26	60.69	60.28
standard conditions.(DSCF)	52.39	57.29	57.09
Total sampling time....(MIN)	60.00	60.00	60.00
Nozzle diameter.....(IN)	.247	.247	.247
Avg.stack gas temp ..(DEG-F)	301	313	321
Volumetric flow rate.....			
actual.....(ACFM)	283059	312014	310072
dry standard.....(DSCFM)	171211	182659	179781
Isokinetic variation.....(%)	101.2	103.7	105.0
Particulate concentration...			
actual.....(GR/ACF)	0.00609	0.00470	0.00501
dry standard.....(GR/DSCF)	0.01007	0.00803	0.00865
Particle mass rate...(LB/HR)	14.781	12.566	13.327
F-factor(DSCF/MMBTU)	9780	9780	9780
Emission factor...(LB/MMBTU)	0.019	0.015	0.017

Test No. 8
Fine Crusher Stack

Results of Particulate Loading Determinations-----Method 5

	Run 1 01-13-95	Run 2 01-13-95	Run 3 01-13-95
Date of run			
Time run start/end.....(HRS)	810/ 917	1000/1105	1124/1230
Static pressure.....(IN.WC)	-0.25	-0.25	-0.25
Cross sectional area (SQ.FT)	5.67	5.67	5.67
Pitot tube coefficient.....	.840	.840	.840
Water in sample gas			
condenser.....(ML)	0.0	0.0	0.0
impingers.....(GRAMS)	1.0	1.0	2.0
desiccant.....(GRAMS)	15.0	14.0	15.0
total.....(GRAMS)	16.0	15.0	17.0
Total particulate material..			
.....collected(grams)	0.0233	0.0173	0.0094
Gas meter coefficient.....	0.9932	0.9932	0.9932
Barometric pressure..(IN.HG)	29.02	29.02	29.02
Avg. orif.pres.drop..(IN.WC)	2.56	2.61	2.67
Avg. gas meter temp..(DEF-F)	51.1	57.2	59.5
Volume through gas meter....			
at meter conditions...(CF)	54.72	55.52	56.45
standard conditions.(DSCF)	54.79	54.94	55.62
Total sampling time....(MIN)	60.00	60.00	60.00
Nozzle diameter.....(IN)	.250	.250	.250
Avg.stack gas temp ..(DEG-F)	69	68	67
Volumetric flow rate.....			
actual.....(ACFM)	16053	16039	16203
dry standard.....(DSCFM)	15313	15354	15512
Isokinetic variation.....(%)	99.3	99.3	99.5
Particulate concentration...			
actual.....(GR/ACF)	0.00626	0.00465	0.00250
dry standard.....(GR/DSCF)	0.00656	0.00486	0.00261
Particle mass rate...(LB/HR)	0.861	0.639	0.347

Test No. 9
Dry Cobber Stack

Results of Particulate Loading Determinations-----Method 5

	Run 1 01-13-95	Run 2 01-13-95	Run 3 01-13-95
Date of run			
Time run start/end.....(HRS)	820/ 921	1000/1105	1124/1226
Static pressure.....(IN.WC)	-0.85	-0.85	-0.85
Cross sectional area (SQ.FT)	20.46	20.46	20.46
Pitot tube coefficient.....	.840	.840	.840
Water in sample gas			
condenser.....(ML)	0.0	0.0	0.0
impingers.....(GRAMS)	-2.0	-3.0	-5.0
desiccant.....(GRAMS)	8.0	14.0	7.0
total.....(GRAMS)	6.0	11.0	2.0
Total particulate material..			
.....collected(grams)	0.0152	0.0116	0.0063
Gas meter coefficient.....	1.0004	1.0004	1.0004
Barometric pressure..(IN.HG)	29.02	29.02	29.02
Avg. orif.pres.drop..(IN.WC)	1.02	1.06	1.06
Avg. gas meter temp..(DEF-F)	72.6	75.1	76.6
Volume through gas meter....			
at meter conditions...(CF)	35.25	35.93	36.01
standard conditions.(DSCF)	33.98	34.48	34.46
Total sampling time....(MIN)	60.00	60.00	60.00
Nozzle diameter.....(IN)	.182	.182	.182
Avg.stack gas temp ..(DEG-F)	71	68	67
Volumetric flow rate.....			
actual.....(ACFM)	67972	68148	67852
dry standard.....(DSCFM)	64878	65040	65558
Isokinetic variation.....(%)	98.9	100.1	99.3
Particulate concentration...			
actual.....(GR/ACF)	0.00659	0.00495	0.00272
dry standard.....(GR/DSCF)	0.00690	0.00519	0.00282
Particle mass rate...(LB/HR)	3.838	2.894	1.585

3.3 Results of Sulfur Dioxide Determinations

Test No. 4
 No. 1205 Waste Gas Stack

Results of Sulfur Dioxide Determinations-----Method 6

	Run 1	Run 2	Run 3
Date of run	01-11-95	01-11-95	01-11-95
Time run start/end.....(HRS)	0840-0940	1022-1125	1153-1253
Barometric pressure..(IN.HG)	29.02	29.02	29.02
Meter temperature....(DEG-F)	70.60	81.90	86.70
Meter correction coefficient	1.0015	1.0015	1.0015
Volume through gas meter....			
at meter conditions...(CF)	47.330	49.210	47.820
standard conditions...(SCF)	45.962	46.807	45.068
Total sampling time....(MIN)	60.0	60.0	60.0
Moisture content.....(%V/V)	13.18	18.07	18.92
Oxygen content....(%V/V DRY)	16.80	16.80	17.00
Milliequivalents of SO4 in..			
gas sample.....	0.1270	0.1020	0.1530
<u>Sulfur dioxide concentration</u>			
(GR/DSCF).....	0.0014	0.0011	0.0017
(MG/DSCM).....	3	2	4
(PPM-DRY).....	1	1	1
(PPM-WET).....	1	1	1
SO2 Emission rate....(LB/HR)	0.77	0.59	0.89

Test No. 7
No. 2 Boiler Stack

Results of Sulfur Dioxide Determinations-----Method 6

	Run 1	Run 2	Run 3
Date of run	01-12-95	01-12-95	01-12-95
Time run start/end.....(HRS)	0917-1017	1047-1147	1217-1322
Barometric pressure..(IN.HG)	28.94	28.94	28.94
Meter temperature....(DEG-F)	73.60	86.60	84.70
Meter correction coefficient	1.0026	1.0026	1.0026
Volume through gas meter....			
at meter conditions...(CF)	54.260	60.690	60.280
standard conditions..(SCF)	52.393	57.291	57.094
Total sampling time....(MIN)	60.0	60.0	60.0
Moisture content.....(%V/V)	9.67	11.18	11.09
Oxygen content....(%V/V DRY)	5.60	5.50	5.80
Milliequivalents of SO4 in..			
gas sample.....	26.6000	28.4000	27.8000
<u>Sulfur dioxide concentration</u>			
(GR/DSCF).....	0.2509	0.2450	0.2407
(MG/DSCM).....	574	561	551
(PPM-DRY).....	216	211	207
(PPM-WET).....	195	187	184
SO2 Emission rate....(LB/HR)	368.27	383.61	370.86
Sulfur dioxide emission.....			
.....factor (LB/MMBTU)*	0.479	0.465	0.465

* F = 9780 DSCF/MMBTU

3.4 Results of Oxides of Nitrogen Determinations

Test No. 4
No. 1205 Waste Gas Stack

Results of Oxides of Nitrogen (NOx) Determinations-----Method 7

	Run 1A	Run 1B	Run 1C	Run 1D
Date of run.....	01-11-95	01-11-95	01-11-95	01-11-95
Time of run.....(HRS)	851	900	920	941
Flask number.....	1	2	3	4
Volume of flask.....(ML)	2086	2063	2055	2116
Data: time of sampling				
flask temperature..(DEG-F)	70.00	71.00	68.00	71.00
bar. press.....(IN.HG)	29.02	29.02	29.02	29.02
flask vacuum.....(IN.HG)	26.10	26.20	26.20	26.40
flask abs. press...(IN.HG)	2.92	2.82	2.82	2.62
Data: Time of Flask Opening				
flask temperature..(DEG-F)	72.00	72.00	72.00	72.00
lab. bar. press....(IN.HG)	29.24	29.24	29.24	29.24
flask static press.(IN.HG)	-1.10	-0.10	-0.10	-0.70
flask abs. press...(IN.HG)	28.14	29.14	29.14	28.54
Volume gas sampled....(DSML)	1723	1778	1770	1797
Moisture content.....(%V/V)	13.18	13.18	13.18	13.18
Nitrate in gas sample...(JG)	550.0	555.0	550.0	585.0
NO2 in gas sample.....(JG)	408.1	411.8	408.1	434.1
<u>NOx Concentration</u>				
(GR/DSCF).....	0.1035	0.1012	0.1007	0.1056
(MG/DSCM).....	237	232	231	242
(PPM-DRY).....	124	121	121	126
(PPM-WET).....	108	105	105	110
NOX Emission rate....(LB/HR)	58.52	57.21	56.95	59.68

Test No. 4
No. 1205 Waste Gas Stack

Results of Oxides of Nitrogen (NOx) Determinations-----Method 7

	Run 2A	Run 2B	Run 2C	Run 2D
Date of run.....	01-11-95	01-11-95	01-11-95	01-11-95
Time of run.....(HRS)	1041	1050	1105	1120
Flask number.....	5	6	7	9
Volume of flask.....(ML)	2057	2100	2081	2080

Data: time of sampling

flask temperature...(DEG-F)	69.00	71.00	70.00	69.00
bar. press.....(IN.HG)	29.02	29.02	29.02	29.02
flask vacuum.....(IN.HG)	26.40	26.40	26.20	26.30
flask abs. press...(IN.HG)	2.62	2.62	2.82	2.72

Data: Time of Flask Opening

flask temperature...(DEG-F)	72.00	72.00	72.00	72.00
lab. bar. press....(IN.HG)	29.24	29.24	29.24	29.24
flask static press.(IN.HG)	1.50	1.90	-1.80	-0.60
flask abs. press...(IN.HG)	30.74	31.14	27.44	28.64
Volume gas sampled....(DSML)	1894	1962	1678	1765
Moisture content.....(%V/V)	18.07	18.07	18.07	18.07
Nitrate in gas sample...(JG)	525.0	575.0	500.0	495.0
NO2 in gas sample.....(JG)	389.5	426.6	371.0	367.3

NOx Concentration

(GR/DSCF).....	0.0899	0.0950	0.0966	0.0909
(MG/DSCM).....	206	217	221	208
(PPM-DRY).....	108	114	116	109
(PPM-WET).....	88	93	95	89
NOx Emission rate....(LB/HR)	49.10	51.90	52.78	49.66

Test No. 4
 No. 1205 Waste Gas Stack

Results of Oxides of Nitrogen (NOx) Determinations-----Method 7

	Run 3A	Run 3B	Run 3C	Run 3D
Date of run.....	01-11-95	01-11-95	01-11-95	01-11-95
Time of run.....(HRS)	1202	1214	1230	1242
Flask number.....	10	11	12	8
Volume of flask.....(ML)	2063	2062	2111	2088
Data: time of sampling				
flask temperature..(DEG-F)	69.00	70.00	70.00	69.00
bar. press.....(IN.HG)	29.02	29.02	29.02	29.02
flask vacuum.....(IN.HG)	26.40	26.30	26.30	26.30
flask abs. press...(IN.HG)	2.62	2.72	2.72	2.72
Data: Time of Flask Opening				
flask temperature..(DEG-F)	72.00	72.00	72.00	72.00
lab. bar. press....(IN.HG)	29.24	29.24	29.24	29.24
flask static press.(IN.HG)	-0.30	-0.50	0.10	0.10
flask abs. press...(IN.HG)	28.94	28.74	29.34	29.34
Volume gas sampled....(DSML)	1778	1757	1841	1820
Moisture content.....(%V/V)	18.92	18.92	18.92	18.92
Nitrate in gas sample...(JG)	595.0	565.0	530.0	520.0
NO2 in gas sample.....(JG)	441.5	419.2	393.2	385.8
<u>NOx Concentration</u>				
(GR/DSCF).....	0.1085	0.1043	0.0934	0.0926
(MG/DSCM).....	248	239	214	212
(PPM-DRY).....	130	125	112	111
(PPM-WET).....	105	101	91	90
NOX Emission rate....(LB/HR)	57.62	55.37	49.57	49.19

3.5 Results of Opacity Observations

Interpoll Labs Report No. 5-4664
Northshore Mining Company
Silver Bay, Minnesota

Test No. 1
Bin Storage

Results of Opacity Observations ----- EPA Method 9*

Percent Opacity	Optical Density	Relative Frequency(%)
0	.0000	
5	.0223	
10	.0458	
15	.0706	
20	.0969	
25	.1249	
30	.1549	
35	.1871	
40	.2219	
45	.2596	
50	.3010	
55	.3468	
60	.3979	
65	.4559	
70	.5229	
75	.6021	
80	.6990	
85	.8239	
90	1.0000	
95	1.3010	
99	2.0000	

Observer: Jeff Scriptor
Cert. Date: 10-9-94
Date of Observation: 1-10-95
Time of Observation: 0830-

- * Could not read visible emissions due to poor weather conditions.

Test No. 7
No. 2 Boiler Stack

Results of Opacity Observations ----- EPA Method 9*

Percent Opacity	Optical Density	Relative Frequency(%)
0	.0000	
5	.0223	
10	.0458	
15	.0706	
20	.0969	
25	.1249	
30	.1549	
35	.1871	
40	.2219	
45	.2596	
50	.3010	
55	.3468	
60	.3979	
65	.4559	
70	.5229	
75	.6021	
80	.6990	
85	.8239	
90	1.0000	
95	1.3010	
99	2.0000	

Observer: Jeff Scriptor
Cert. Date: 10-9-94
Date of Observation: 1-12-95
Time of Observation: 0920-

- * Visible emissions observations could not be performed due to poor weather conditions.

Interpoll Labs Report No. 5-4664
Northshore Mining Company
Silver Bay, Minnesota

Test No. 9
Dry Cobber Stack

Results of Opacity Observations ----- EPA Method 9*

Percent Opacity	Optical Density	Relative Frequency(%)
0	.0000	
5	.0223	
10	.0458	
15	.0706	
20	.0969	
25	.1249	
30	.1549	
35	.1871	
40	.2219	
45	.2596	
50	.3010	
55	.3468	
60	.3979	
65	.4559	
70	.5229	
75	.6021	
80	.6990	
85	.8239	
90	1.0000	
95	1.3010	
99	2.0000	

Observer: Jeff Scriptor
Cert. Date: 10-9-94
Date of Observation: 1-13-95
Time of Observation: 0820-

* Visible emissions observations could not be performed due to poor weather conditions.

APPENDIX A

VOLUMETRIC FLOW RATE DETERMINATIONS

Test No. 1
Bin Storage Stack

Results of Volumetric Flow Rate Determination-----Method 2

Date of Determination.....	01-10-95
Time of Determination.....(HRS)	750
Barometric pressure.....(IN.HG)	29.46
Pitot tube coefficient.....	.84
Number of sampling ports.....	2
Total number of points.....	24
Shape of duct.....	Round
Stack diameter.....(IN)	39.5
Duct area.....(SQ.FT)	8.51
Direction of flow.....	UP
Static pressure.....(IN.WC)	-.65
Avg. gas temp.....(DEG-F)	65
Moisture content.....(% V/V)	0.99
Avg. linear velocity.....(FT/SEC)	58.7
Gas density.....(LB/ACF)	.07377
Molecular weight.....(LB/LBMOLE)	28.84
Mass flow of gas.....(LB/HR)	132684
Volumetric flow rate.....	
actual.....(ACFM)	29976
dry standard.....(DSCFM)	29344

Test No. 3
No. 1104 Pelletizer Stack

Results of Volumetric Flow Rate Determination-----Method 2

Date of Determination.....	01-10-95
Time of Determination.....(HRS)	750
Barometric pressure.....(IN.HG)	29.38
Pitot tube coefficient.....	.84
Number of sampling ports.....	4
Total number of points.....	24
Shape of duct.....	Round
Stack diameter.....(IN)	71
Duct area.....(SQ.FT)	27.49
Direction of flow.....	UP
Static pressure.....(IN.WC)	-.14
Avg. gas temp.....(DEG-F)	126
Moisture content.....(% V/V)	15.00
Avg. linear velocity.....(FT/SEC)	56.7
Gas density.....(LB/ACF)	.06280
Molecular weight.....(LB/LBMOLE)	28.99
Mass flow of gas.....(LB/HR)	352711
Volumetric flow rate.....	
actual.....(ACFM)	93605
dry standard.....(DSCFM)	70367

Test No. 5
No. 1204 Waste Gas Stack

Results of Volumetric Flow Rate Determination-----Method 2

Date of Determination.....	01-11-95
Time of Determination.....(HRS)	745
Barometric pressure.....(IN.HG)	29.02
Pitot tube coefficient.....	.84
Number of sampling ports.....	4
Total number of points.....	24
Shape of duct.....	Round
Stack diameter.....(IN)	71.5
Duct area.....(SQ.FT)	27.88
Direction of flow.....	UP
Static pressure.....(IN.WC)	.26
Avg. gas temp.....(DEG-F)	136
Moisture content.....(% V/V)	18.06
Avg. linear velocity.....(FT/SEC)	55.1
Gas density.....(LB/ACF)	.06030
Molecular weight.....(LB/LBMOLE)	28.99
Mass flow of gas.....(LB/HR)	333598
Volumetric flow rate.....	
actual.....(ACFM)	92202
dry standard.....(DSCFM)	64958

Test No. 6
 Rotoclone Stack

Results of Volumetric Flow Rate Determination-----Method 2

Date of Determination.....	01-12-95
Time of Determination.....(HRS)	810
Barometric pressure.....(IN.HG)	28.94
Pitot tube coefficient.....	.84
Number of sampling ports.....	2
Total number of points.....	20
Shape of duct.....	Round
Stack diameter.....(IN)	45.5
Duct area.....(SQ.FT)	11.29
Direction of flow.....	UP
Static pressure.....(IN.WC)	-.82
Avg. gas temp.....(DEG-F)	143
Moisture content.....(% V/V)	6.11
Avg. linear velocity.....(FT/SEC)	63.2
Gas density.....(LB/ACF)	.06184
Molecular weight.....(LB/LBMOLE)	28.84
Mass flow of gas.....(LB/HR)	158912
Volumetric flow rate.....	
actual.....(ACFM)	42831
dry standard.....(DSCFM)	33987

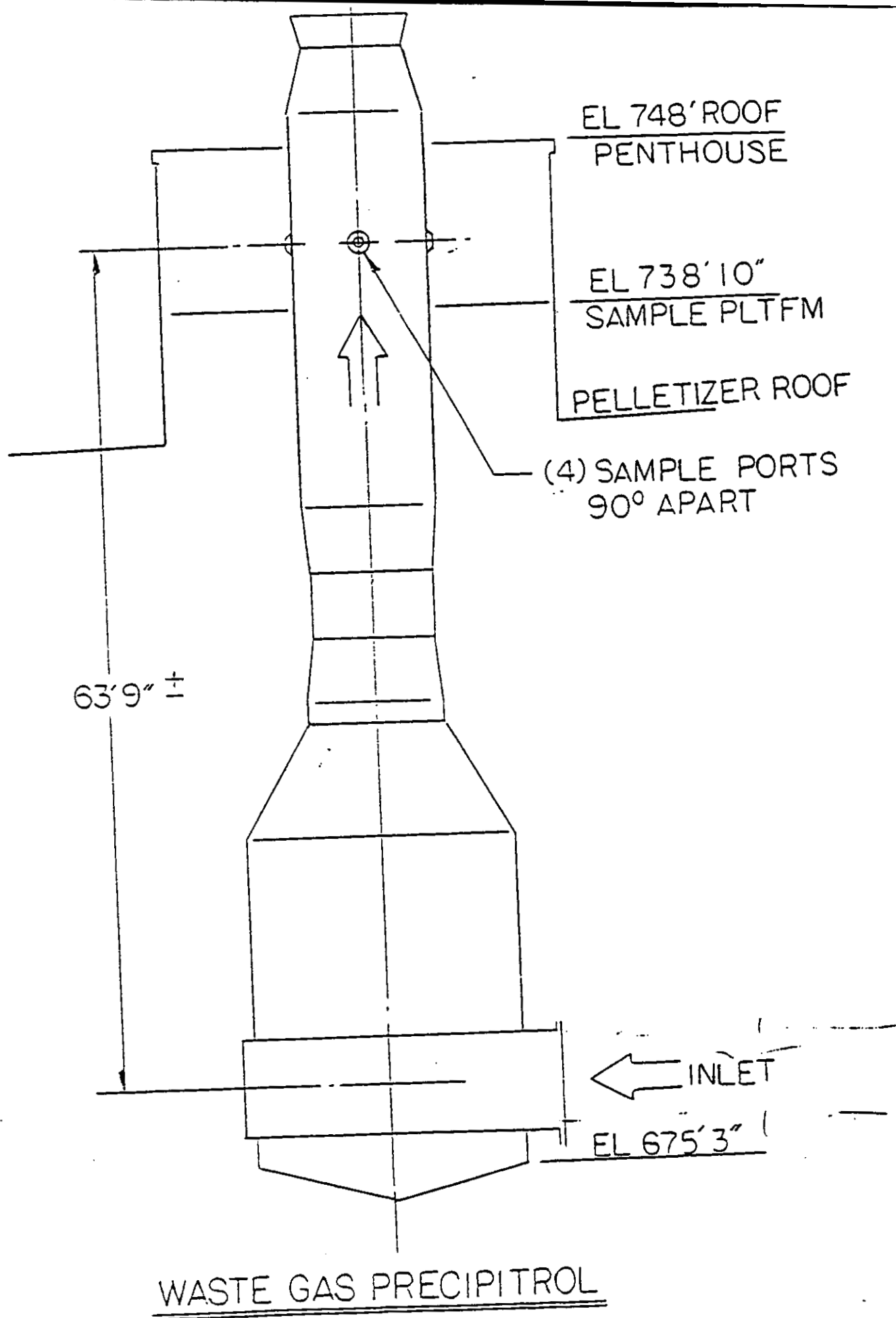
Test No. 8
Fine Crusher Stack

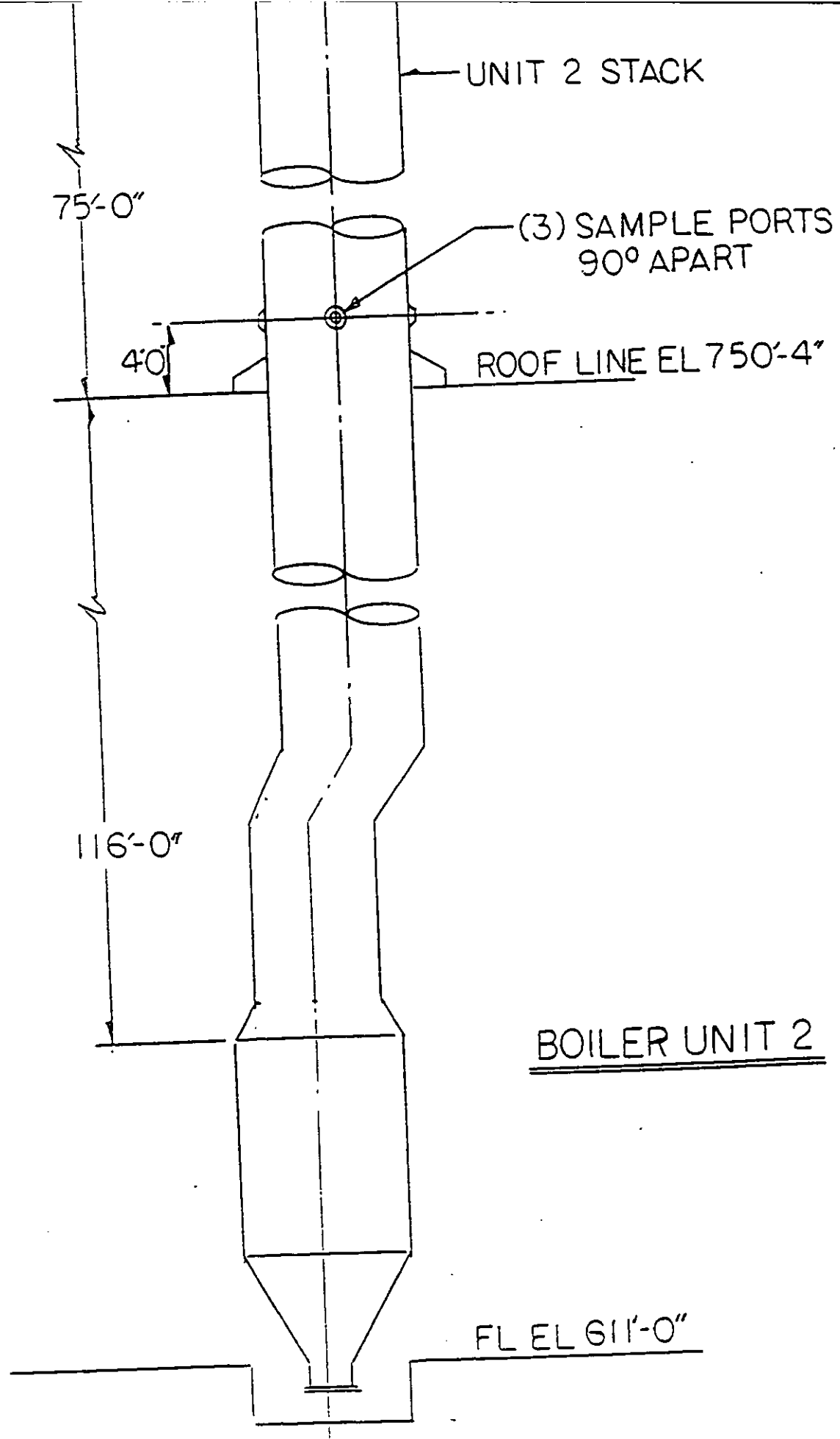
Results of Volumetric Flow Rate Determination-----Method 2

Date of Determination.....	01-13-95
Time of Determination.....(HRS)	750
Barometric pressure.....(IN.HG)	29.02
Pitot tube coefficient.....	.84
Number of sampling ports.....	2
Total number of points.....	12
Shape of duct.....	Round
Stack diameter.....(IN)	32.25
Duct area.....(SQ.FT)	5.67
Direction of flow.....	UP
Static pressure.....(IN.WC)	-.25
Avg. gas temp.....(DEG-F)	86
Moisture content.....(% V/V)	1.36
Avg. linear velocity.....(FT/SEC)	46.4
Gas density.....(LB/ACF)	.06985
Molecular weight.....(LB/LBMOLE)	28.84
Mass flow of gas.....(LB/HR)	66227
Volumetric flow rate.....	
actual.....(ACFM)	15803
dry standard.....(DSCFM)	14612

APPENDIX B

LOCATION OF TEST PORTS



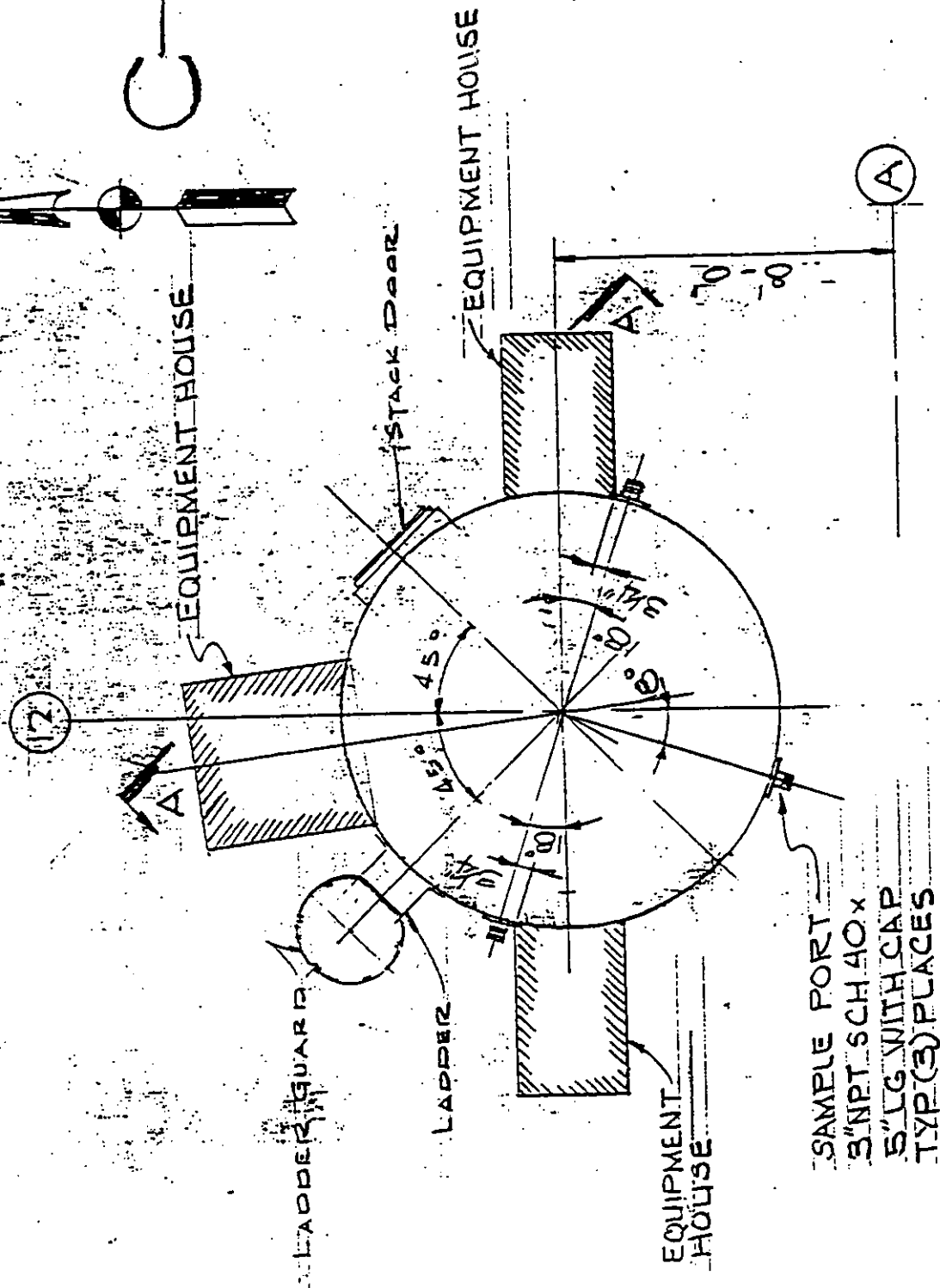


554-110

PLANT NORTH

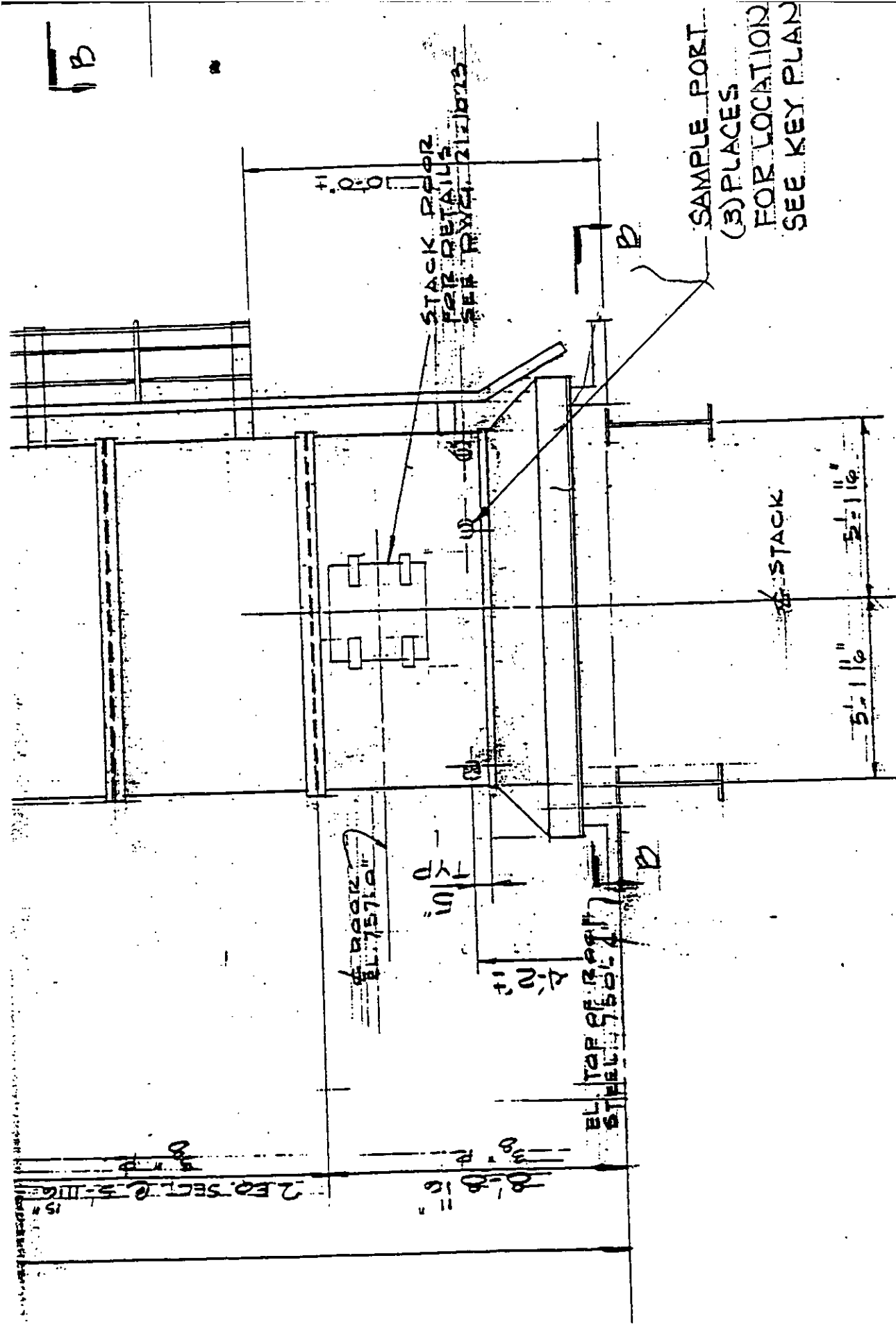
TYPICAL)
DASHED (TYP.)

B-3



Y
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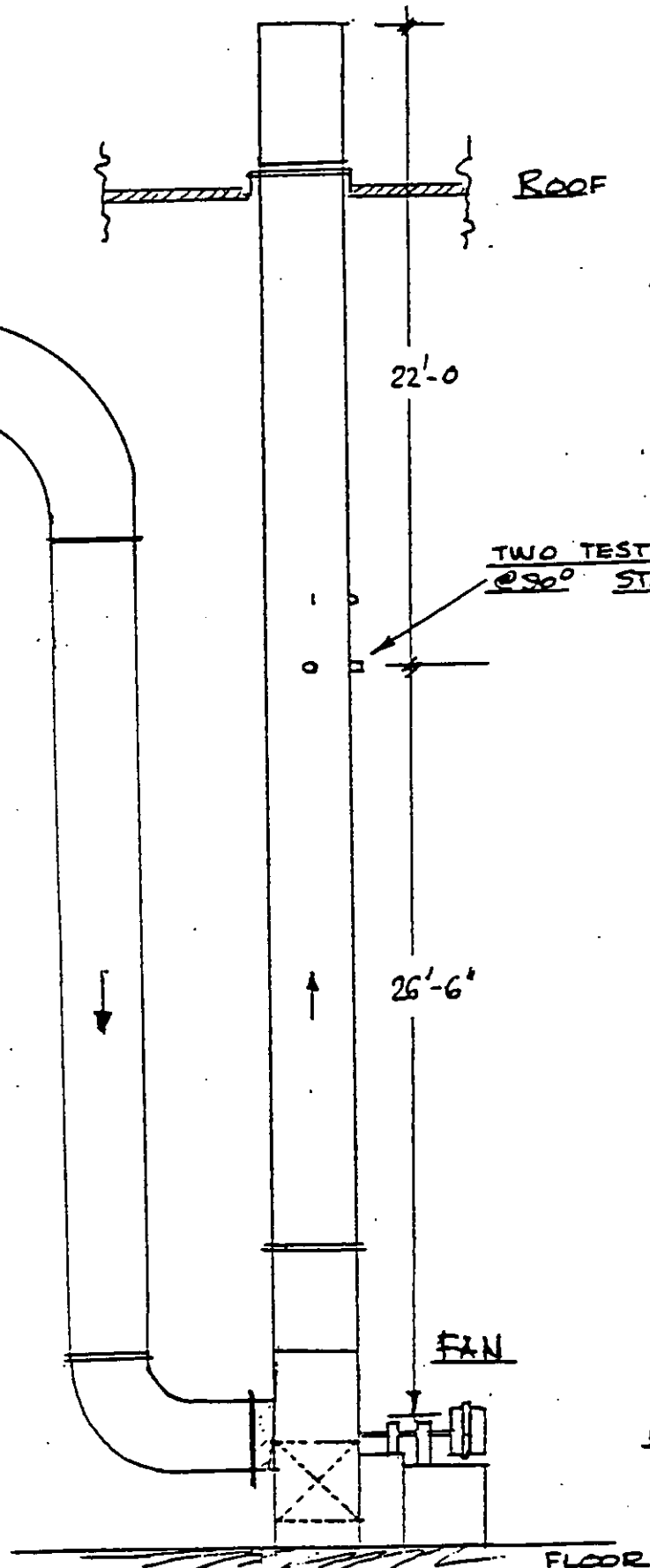
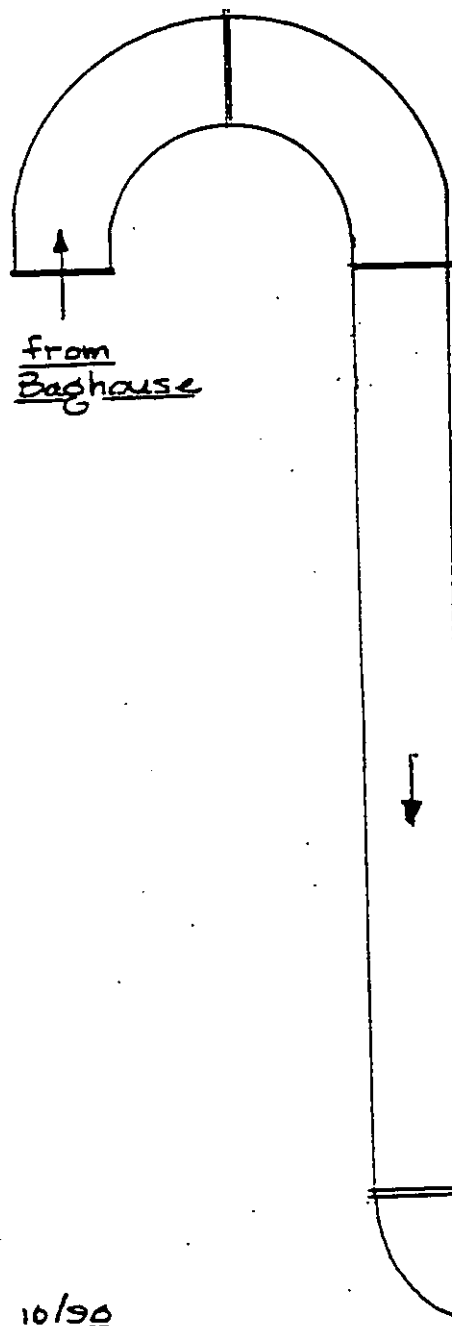
SILVER BAY MINN.



ELEVATION A-A

LOOKING SOUTHWEST - SEE KEY PLAN
 DRAWING SCALE: 1/4" = 1'-0"

LP 10/90



NOT TO SCALE

APPENDIX C

FIELD DATA SHEETS

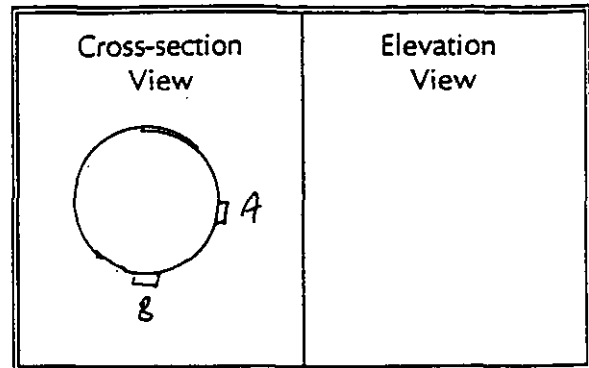
INTERPOL LABORATORIES, INC.

(612) 786-6020

EPA Method 2 Field Data Sheet

Drawing of Test Site

Job NORTHSHORE MINING
 Source 3:14 STEADY STATE STACK
 Test 1 Run / Date 1-10-75
 Stack Dimen. 37 1/2 IN.
 Dry Bulb °F Wet bulb °F
 Manometer ☒ Reg. ☐ Exp ☐ Elec.
 Barometric Pressure 29.416 IN.HG
 Static Pressure -1.65 IN.WC
 Operators EITROW BLIDGE -
 Pitot No. 271-4 C. 1.84



Traverse Point No.	Fraction of Diameter	Distance From Stack Wall (IN.)	Distance From End of Port (IN.)	Velocity	Temp. of Gas (°F)
		Port Length: <u>4.5</u> IN.	Time Start: <u>0750</u> HRS		
1	.081	.83	5.33	1.10	
2	.067	2.65	7.15	1.20	
3	.118	4.66	9.16	1.20	
4	.177	6.97	11.47	1.20	
5	.250	9.88	14.38	1.20	
6	.356	14.06	18.56	1.15	65
7	.644	25.44	29.94	1.15	
8	.750	29.63	34.13	1.20	
9	.823	32.51	37.01	1.10	
10	.882	34.84	39.34	1.10	
11	.933	36.85	41.35	1.05	
12	.979	38.67	43.17	1.05	
13				1.90	
2				1.05	
3				1.10	
4				1.10	
5				1.10	
6				1.15	64
7				1.15	
8				1.10	
9				1.00	
10				1.90	
11				1.90	
12				1.75	
Temp. Meas. Device & S/N: <u>PDT-34</u>				Time End: <u>0825</u> HRS	

R or nothing = reg. manometer; S = expanded; E = electronic

032594-G:STACKWPAFORMSS-392.1

INTERPOLL LABORATORIES, INC.

(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job NORTHSHORE MINING Date 1-10-95 Test 1 Run 1
 Source BIN STORAGE STACK No. of traverse points 24
 Method 5 Filter holder: 4" GLASS Filter type: 4" GF

Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 IN.HG (vac) ☒
 Post test: 0 cfm at 15 IN. HG (vac) ☒

Particulate Catch Data:

No. of filters used:

Recovery solvent(s)

6756☒ acetone☐ other(s)

No. of probe wash bottles:

Sample recovered by:

ET

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2	<u>200</u>	<u>100</u>	<u>0</u>
Impinger No. 3		<u>0</u>	
Condenser			
Desiccant	<u>1451</u>	<u>1473</u>	<u>8</u>
Total			<u>8</u>

Integrated Gas Sampling Data:

Bag Pump No. _____
 Bag Material: 5-layer Aluminized Tedlar
 Pretest leak check: _____
 Time start: _____
 Sampling rate: _____

Box No. N/A Bag No. _____
 Size: 44 L
 cc/min at _____ IN.HG
 (HRS) Time end: _____ (HRS)
 cc/min Operator: _____

S/N of O₂ Analyzer used to monitor train outlet: _____

052394-G:STACKWPIFORMSIS-0046RR

EPA Method 5 Field Data Sheet

Job WORTHSHORE MINING
 Source BEAR STAR ROSS STRUCK
 Date 1-10-85 Test 1 Run 1

Operators 57-JB-JS
 Meter Box No. 3 ΔH @ 1.75 in. WC
 Gas meter Coeff. 1.0004

Nozzle No. 3-3
 Nozzle Dia. 1.86 in.
 Bar. Press. 24.46 in. Hg

Pilot No. 2914
 C_p .84
 H₂O %

Source		Date		1-10-45- Test		Run		1,0004		Bar. Press.		27.86 in. Hg			
Traverse Point No.	Sampling Time (min)	Sample Vol. (cf)	Velocity Head (in. WC)	Orifice Meter (in. WC)	Des. Vol. (cf)	VAC. (in. Hg)	Temperatures (°F)					Oxygen (% v/v)			
							Stack	Probe	Oven	Imp.	Gas/In		Gas/Out		
	0530	763.20													
A 12	2.5	764.70	1.90	1.07	4.67	3.5	65				36	5.2	50		
11	5	766.30	1.00	1.17	4.20	3.5	65					5.4	51		
10	7.5	767.90	1.10	1.29	7.81	4.0	45				36	5.7	51		
9	10	769.50	1.10	1.31	9.43	4.0	40				36	5.9	51		
8	12.5	771.18	1.15	1.37	1.09	4.0	40					5.9	51		
7	15	772.93	1.15	1.38	2.75	4.0	56				36	6.1	53		
6	17.5	774.36	1.10	1.33	4.39	3.5	56				36	6.4	54		
5	20	776.44	1.12	1.35	6.05	4.0	58				37	6.5	54		
4	22.5	777.70	1.10	1.33	7.69	4.0	58					6.6	55		
3	25	779.32	1.10	1.33	9.33	4.0	57				37	6.7	55		
2	27.5	780.97	1.05	1.28	8.94	4.0	57					6.8	56		
1	30	782.10	1.85	1.03	2.39	3.3	57				36	6.6	56		
B 12	32.5	783.72	1.65	1.79	3.66	2.5	58					6.8	57		
11	35	784.98	1.70	1.85	4.98	2.8	56				36	6.9	57		
10	37.5	786.40	1.75	1.91	4.35	3.0	56					7.0	57		
9	40	787.86	1.85	1.04	7.81	3.5	56				35	7.0	58		
8	42.5	789.52	1.10	1.35	9.46	4.0	56					7.0	58		
7	45	791.24	1.15	1.41	1.16	4.3	56				35	7.1	58		
6	47.5	792.90	1.15	1.41	2.85	4.3	56					7.1	58		
5	50	794.60	1.10	1.35	4.52	4.0	56				35	7.1	58		
4	52.5	796.22	1.10	1.35	6.18	4.0	56					7.1	59		
3	55	797.85	1.10	1.35	7.83	4.0	57				35	7.1	59		
2	57.5	799.40	1.05	1.29	9.46	3.8	57					7.1	59		
1	60	801.03	1.95	1.16	1.00	3.5	56					7.1	59		
		0938													
		0 - 60													
		V _m - 37.83		ΔH - 1.23											

INTERPOLL LABORATORIES, INC.

(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job NORTHSHORE MINING Date 1-10-95 Test 1 Run 2
 Source BIN STORAGE STACK No. of traverse points 24
 Method 5 Filter holder: 4" GLASS Filter type: 4" GF

Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 IN.HG (vac) ☒
 Post test: 0 cfm at 15 IN. HG (vac) ☒

Particulate Catch Data:

No. of filters used:

Recovery solvent(s)

6755

☒ Acetone _____
☐ other(s) _____

No. of probe wash bottles:

Sample recovered by:

1
ET

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1		<u>100</u>	
Impinger No. 2	<u>200</u>	<u>100</u>	<u>0</u>
Impinger No. 3		<u>0</u>	
Condenser			
Desiccant	<u>1450</u>	<u>1460</u>	<u>10</u>
Total			<u>10</u>

Integrated Gas Sampling Data:

Bag Pump No. _____
 Bag Material: 5-layer Aluminized Tedlar
 Pretest leak check: _____
 Time start: _____
 Sampling rate: _____

N/A
 Box No. _____ Bag No. _____
 Size: 44 L
 cc/min at _____ IN.HG
 (HRS) Time end: _____ (HRS)
 cc/min Operator: _____

S/N of O₂ Analyzer used to monitor train outlet: _____

052394-G:STACK\WP\FORMS\SS-0046RR

(612) 786-6020

EPA Method 5 Field Data Sheet

 Job
 Source
 Date

 NORTHSHORE MANUFACTURING
 131N SHORELINE STREET
 1-10-83

 Operators
 Meter Box No.
 Gasometer Coeff.

 57-J6-JS
 3 ΔH@ 1.73 in.WC
 1.0004

 Nozzle No.
 Nozzle Dia.
 Bar. Press.

 3-3
 1.86 in.
 29.46 in.Hg

 Pilot No.
 C_p
 H₂O

 29V-4
 1.84
 1

Traverse Point No.	Sampling Time (min)	Sample Vol. (cf)	Velocity Head (in.WC)	Orifice Meter (in.WC)	Des. Vol. (cf)	VAC. (in.Hg)	Temperatures (°F)					Oxygen (% v/v)	
							Stack	Probe	Oven	Imp.	Gas/In		Gas/Out
13	0958	801.30											
12	7.5	802.90	1.95	1.16	2.83	4.0	57			35	62	57	
11	5	804.50	1.10	1.34	4.48	4.5	57			35	64	57	
10	7.5	806.19	1.10	1.34	6.13	4.5	57			35	45	57	
9	10	807.84	1.10	1.34	7.78	4.5	57				64	58	
8	14.5	809.55	1.12	1.37	9.45	4.5	57			36	67	58	
7	15	811.20	1.10	1.35	1.11	4.5	57				68	58	
6	17.5	812.90	1.15	1.41	2.80	4.6	57			36	69	59	
5	20	814.50	1.05	1.29	4.43	4.3	57				69	59	
4	22.5	816.10	1.05	1.29	6.06	4.3	57			36	70	59	
3	25	817.74	1.05	1.29	7.68	4.3	57				71	59	
2	27.5	819.30	1.05	1.30	9.31	4.3	57			36	71	59	
1	30	820.90	1.00	1.24	1.91	4.0	56			44	71	60	
13	32.5	822.40	1.90	1.11	2.42	4.0	57				71	60	
11	35	824.07	1.10	1.36	4.09	4.5	57				72	60	
10	37.5	825.72	1.10	1.36	5.76	4.5	57			44	72	61	
9	40	827.38	1.12	1.39	7.44	4.7	57				72	61	
8	42.5	829.08	1.12	1.39	9.13	4.7	57			50	73	61	
7	45	830.80	1.10	1.37	0.81	4.7	56				72	61	
6	47.5	832.50	1.10	1.36	2.48	4.7	56			50	73	62	
5	50	834.15	1.20	1.49	4.23	4.4	56				73	62	
4	51.5	835.99	1.15	1.43	5.94	4.8	56			50	73	62	
3	55	837.70	1.10	1.37	7.62	4.7	56			50	73	62	
2	57.5	839.40	1.15	1.43	9.34	4.8	56			50	73	62	
1	60	840.90	1.90	1.12	1.85	4.0	57				73	62	
	(1102)												
	0-60	V _m - 39.60		ΔH - 1.35							AVG. 44.9		

INTERPOLL LABORATORIES, INC.

(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job NORTHSHORE MINING Date 1-10-95 Test 1 Run 3
 Source BIN STORAGE STACK No. of traverse points 24
 Method 5 Filter holder: 4" GLASS Filter type: 4" GF

Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 IN. HG (vac) ☒
 Post test: 0 cfm at 5 IN. HG (vac) ☒

Particulate Catch Data:

No. of filters used:

Recovery solvent(s)

10759

☒ acetone _____
☐ other(s) _____

No. of probe wash bottles:

Sample recovered by:

1
ET

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1		<u>(100)</u>	
Impinger No. 2	<u>200</u>	<u>(100)</u>	<u>0</u>
Impinger No. 3		<u>0</u>	
Condenser			
Desiccant	<u>1459</u>	<u>1481</u>	<u>8</u>
Total			<u>8</u>

Integrated Gas Sampling Data:

Bag Pump No. _____
 Bag Material: 5-layer Aluminized Tedlar
 Pretest leak check: _____
 Time start: _____
 Sampling rate: _____

Box No. N/A Bag No. _____
 Size: 44 L
 cc/min at _____ IN. HG
 (HRS) Time end: _____ (HRS)
 cc/min Operator: _____

S/N of O₂ Analyzer used to monitor train outlet: _____

052394-G:STACK\WP\FORMS\S-0046RR

EPA Method 5 Field Data Sheet

Job NORTHSHORE MINING
 Source BIN STACK RAP STACK
 Date 1-10-93 Test 1 Run 5

Operators
 Meter Box No. 3
 Gasometer Coeff. 1.00004

Nozzle No. 3-3
 Nozzle Dia. 1.182 in.
 Bar. Press. 29.46 in. Hg

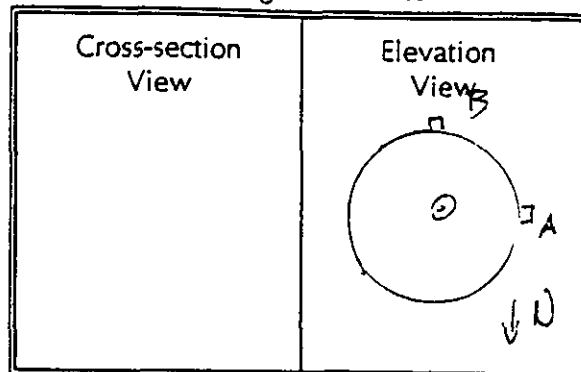
Pilot No. 299-4
 C_p 1.840
 H₂O

Traverse Point No.	Sampling Time (min)	Sample Vol. (cf)	Velocity Head (in. WC)	Orifice Meter (in. WC)	Des. Vol. (cf)	VAC. (in. Hg)	Temperatures (°F)					Oxygen (% v/v)	
							Stack	Probe	Oven	Imp.	Gas/In		Gas/Out
	1116	841.10											
A 12	2.5	842.78	1.05	1.24	2.72	4.1	56			33	62	59	
11	5	844.40	1.05	1.28	4.34	4.1	56				64	59	
10	7.5	846.08	1.10	1.35	6.00	4.2	54			34	65	59	
9	10	847.70	1.10	1.35	7.66	4.2	54				67	59	
8	12.5	849.41	1.12	1.38	9.33	4.3	56			24	67	60	
7	15	851.10	1.20	1.47	1.07	4.8	56				68	60	
6	17.5	852.80	1.15	1.41	2.77	4.7	56			34	69	60	
5	20	854.58	1.20	1.48	4.50	4.8	56				70	61	
4	22.5	856.27	1.20	1.48	6.25	4.8	55			34	70	61	
3	25	857.95	1.10	1.36	7.91	4.7	55			35	70	61	
2	27.5	859.40	1.10	1.36	9.58	4.7	55				71	61	
1	30	861.10	1.85	1.05	1.05	3.5	55			35	71	62	
B 12	32.5	862.70	1.05	1.30	2.69	4.3	55			35	72	62	
11	35	864.40	1.10	1.36	4.36	4.4	55				74	63	
10	37.5	866.09	1.10	1.36	6.04	4.4	56			34	75	63	
9	40	867.78	1.15	1.43	7.76	4.5	56			35	75	64	
8	42.5	869.43	1.10	1.37	9.44	4.4	55			35	75	64	
7	45	871.07	1.10	1.37	1.18	4.4	54			35	75	64	
6	47.5	872.74	1.05	1.31	2.77	4.3	54			35	75	64	
5	50	874.40	1.05	1.31	4.41	4.3	54			35	75	64	
4	52.5	876.05	1.10	1.37	6.10	4.4	54			35	76	64	
3	55	877.70	1.05	1.31	7.74	4.3	56			35	75	65	
2	57.5	879.35	1.05	1.31	9.38	4.3	56			35	75	65	
1	60	880.90	1.85	1.06	8.86		55				75	65	
	(1220)												
	0-60	V _m - 59.80		ΔH 734								Avg. - 64.6	

INTERPOLL LABORATORIES, INC.
(612) 786-6020
EPA Method 2 Field Data Sheet

Drawing of Test Site

Job Corpus North Shore
Source NO 1105 23101.2.1.1 Stack
Test 2 Run Date 11.2.95
Stack Dimen. 71 IN.
Dry Bulb °F Wet bulb °F
Manometer ☐ Reg. ☐ Exp ☐ Elec.
Barometric Pressure 29.38 IN.HG
Static Pressure -2.23 IN.WC
Operators D. Van Housen + E.T. Franzen
Pitot No. 136-6 C₂ .50
PM



Traverse Point No.	Fraction of Diameter	Distance From Stack Wall (IN.)	Distance From End of Port (IN.)	Velocity	Temp. of Gas (°F)
		Port Length: <u>5</u> IN.		Time Start:	HRS
1	.321	1.49	6.47		
2	.067	4.76	9.76		
3	.118	8.34	13.34		
4	.177	12.56	17.56		
5	.25	17.75	22.75		
6	.356	25.27	30.27		
7	.644	45.72	50.72		
8	.75	53.25	58.25		
9	.823	58.43	63.43		
10	.882	62.62	67.62		
11	.939	66.67	71.67		
12	.979	69.5	74.5		
13					
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99					
100					

Temp. Meas. Device & S/N:

PDT # 8 + 35

Time End:

HRS

R or nothing = reg. manometer; S = expanded; E = electronic

INTERPOLL LABORATORIES, INC.

(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job North Shore Date 11/06/95 Test 2 Run 1
 Source No. 1105 Pelletizer Stack No. of traverse points 24
 Method 5 Filter holder: glass Filter type: glass fiber

Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 IN.HG (vac) ☒
 Post test: 0 cfm at 8 IN. HG (vac) ☒

Particulate Catch Data:

No. of filters used:

Recovery solvent(s)

7067

☒ acetone
☐ other(s)

No. of probe wash bottles:

Sample recovered by:

1
D. H. H.

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2	<u>36.7</u>	<u>200</u>	<u>167</u>
Impinger No. 3			
Condenser			
Desiccant	<u>1358</u>	<u>1334</u>	<u>24</u>
Total			<u>191</u>

Integrated Gas Sampling Data:

Bag Pump No. 36A
 Bag Material: 5-layer Aluminized Tedlar
 Pretest leak check: 0
 Time start: 0830
 Sampling rate: 400

Box No. 13 Bag No. 1
 Size: 44 L
 cc/min at 14 IN.HG
 (HRS) Time end: 0932 (HRS)
 cc/min Operator: D.H.H.

S/N of O₂ Analyzer used to monitor train outlet:

36A

052394-G:\STACK\WP\FORMS\S-0046RR

EPA Method 5 Field Data Sheet

Job

Cypress North Shore

Source

No 1105 Pelletizer Stack

Date

1/10/95 Test 2 Run 1

Operators

David & T.F.

Meter Box No.

15 ΔH @ 1.85 in. WC

Gas meter Coeff.

1.0015

Nozzle No.

247 in.

Nozzle Dia.

29.38 in. Hg

Bar. Press.

29.38 in. Hg

Pilot No.

138-6

C₉

54

H₂O

73

Traverse Point No.	Sampling Time (min)	Sample Vol. (cf)	Velocity Head (in. WC)	Orifice Meter (in. WC)	Des. Vol. (cf)	VAC. (in. Hg)	Temperatures (°F)					Gas/In	Gas/Out	Oxygen (% v/v)
							Stack	Probe	Oven	Imp.				
	0627	813.90												
B 12	2.5	816.30	1.05	3.05	6.3	6	135	269	212	40	71	70	15.3	
11	5	818.67	.97	2.84	8.64	6	131				75	69	15.5	
10	7.5	820.85	1.00	2.93	1.01	6	131				74	69	15.5	
9	10	823.31	1.00	2.95	3.40	6	131	263	253	40	81	71	15.9	
8	12.5	825.54	.96	2.84	5.74	6	131				83	71	17.0	
7	15	827.91	.95	2.83	8.08	6	128				83	71	19.3	
6	17.5	830.31	.97	2.90	0.46	6	126	261	257	41	86	72	15.5	
5	20	832.58	.82	2.46	2.65	5	126				87	73	15.4	
4	21.5	834.85	.77	2.32	4.78	5	125				89	73	15.8	
3	25	836.54	.85	1.66	6.58	5	125	260	256	41	89	73	15.5	
2	21.5	838.43	.50	1.51	8.30	5	125				90	74	15.5	
1	30	839.99	.58	1.45	9.97	5	125				90	75	15.5	
A 12	32.5	841.95	.60	1.82	1.88	5	125	263	257	48	86	75	15.8	
11	35	844.26	.79	2.37	4.03	5	128				91	76	15.5	
10	37.5	846.40	.72	2.77	6.34	6	128				93	76	15.5	
9	40	848.70	.96	2.89	8.75	6	130	260	254	48	94	77	15.5	
8	42.5	851.11	.96	2.89	1.11	6	130				94	77	15.7	
7	45	853.45	.97	2.92	3.54	6	130				95	78	15.7	
6	47.5	855.95	.94	2.84	5.90	6	130	259	256	48	95	78	15.7	
5	50	858.30	.95	2.88	8.29	6	127				96	78	15.9	
4	52.5	860.80	.96	2.92	0.67	6	127				96	79	15.8	
3	55	863.17	.95	2.89	3.08	6	127	257	258	47	97	79	15.7	
2	57.5	865.43	.93	2.81	5.43	6	131				97	80	15.7	
1	60	867.50	.77	2.33	7.59	5	131				97	80	15.7	
	10032													
	0-60	V _m - 53.60		ΔH - 2.59										
												</		

INTERPOL LABORATORIES, INC.

(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job North Shore Date 1/10/15 Test 2 Run 2
 Source AD 1105 Pellet 120 Stack No. of traverse points 24
 Method 5 Filter holder: glass Filter type: glass fiber

Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 IN.HG (vac) ☒
 Post test: 0 cfm at 8 IN. HG (vac) ☒

Particulate Catch Data:

No. of filters used:

Recovery solvent(s)

7068

☒ acetone
☐ other(s)

No. of probe wash bottles:

Sample recovered by:

1

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2	390	200	190
Impinger No. 3			
Condenser			
Desiccant	1324	1305	19
Total			209

Integrated Gas Sampling Data:

Bag Pump No.

36A

Box No.

13 Bag No. 2

Bag Material:

5-layer Aluminized Tedlar

Size:

44 L

Pretest leak check:

0

cc/min at

15 IN.HG

Time start:

1005

(HRS) Time end:

1152 (HRS)

Sampling rate:

702

cc/min Operator:

 S/N of O₂ Analyzer used to monitor train outlet:36A

052394-G:STACKWPF:FORM55-0046RR

EPA Method 5 Field Data Sheet

Job NORTH Shore
 Source NO 105 Rillietree Stack
 Date 1/10/95 Test Q Run 3

Operators

Meter Box No.

Gas meter Coeff.

D.H. & T.F.15 $\Delta H @ 1.85$ in. WC1.0015

Nozzle No.

Nozzle Dia.

Bar. Press.

7-4247 in.29.38 in. Hg

Pilot No.

U 36-687145 %

Traverse Point No.	Sampling Time (min)	Sample Vol. (cf)	Velocity Head (in. WC)	Orifice Meter (in. WC)	Des. Vol. (cf)	VAC. (in. Hg)	Temperatures (°F)					Oxygen (% v/v)		
							Stack	Probe	Oven	Imp.	Gas/In		Gas/Out	
1	1003	867.71												
2	2.5	869.26	6.8	1.94	9.68	4	127	263	270	43		82	79	18.5
3	5	871.51	7.6	2.21	1.76	4	130					84	79	19.2
4	7.5	874.86	9.6	2.79	4.10	5	130					78	77	19.2
5	10	876.25	1.10	3.17	6.58	6	130	261	266	48		85	77	19.2
6	12.5	877.65	1.10	3.19	9.07	6	130					88	78	19.2
7	15	881.31	1.10	3.21	1.58	6	130					87	78	19.2
8	17.5	883.65	1.0	2.98	3.97	6	130	260	267	48		90	78	19.3
9	20	886.00	1.77	2.84	6.33	6	128					91	78	19.5
10	22.5	888.35	98	2.88	8.71	6	128					91	78	19.3
11	25	890.70	97	2.84	1.07	6	130	260	266	48		92	78	19.3
12	27.5	893.00	83	2.42	3.25	5	133					92	79	19.3
13	30	895.88	1.62	1.81	5.14	4	133					93	78	19.4
14	32.5	897.24	97	2.83	7.50	5	133	263	263	49		89	79	19.4
15	35	899.39	1.0	2.94	9.90	6	127					93	77	19.3
16	37.5	901.90	1.10	3.23	2.43	7	128					94	77	19.4
17	40	904.25	1.0	2.94	4.81	6	128	265	260	47		95	77	19.1
18	42.5	906.71	1.10	2.95	7.25	1	128					95	80	19.2
19	45	909.16	1.0	2.95	9.67	6	127					95	80	19.2
20	47.5	911.65	94	2.78	2.01	6	127	260	252	43		95	80	19.5
21	50	914.00	97	2.87	4.39	6	126					95	80	19.5
22	52.5	916.45	97	2.87	6.77	6	126					96	80	19.5
23	55	918.85	95	2.82	9.19	6	126	256	255	44		96	80	19.4
24	57.5	921.09	75	2.22	1.23	5	126					96	80	19.5
25	60	922.63	47	1.40	7.90	3	126					96	80	19.5
26	1152													
27	0-60	54.92		ΔH = 2.7								Avg. = 85		

INTERPOL LABORATORIES, INC.

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Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job North Shore 2 Date 11/10/75 Test 2 Run 3
 Source No 1105 Pelletier Street No. of traverse points 24
 Method 5 Filter holder: 9/255 Filter type: glass fiber

Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 IN.HG (vac) ☐Post test: 0 cfm at 8 IN. HG (vac) ☒

Particulate Catch Data:

No. of filters used:

Recovery solvent(s)

☒ acetone☐ other(s)

No. of probe wash bottles:

Sample recovered by:

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2	380	200	180
Impinger No. 3			
Condenser			
Desiccant	1356	1324	22
Total			202

Integrated Gas Sampling Data:

Bag Pump No.

36 A

Box No.

13 Bag No. 3

Bag Material:

5-layer Aluminized Tedlar

Size:

44 L

Pretest leak check:

0

cc/min at

14 IN.HG

Time start:

1230

(HRS) Time end:

1327 (HRS)

Sampling rate:

400

cc/min Operator:

DLHS/N of O₂ Analyzer used to monitor train outlet:36 A

052394-G:STACK\WP\FORMS\S-0046RR

Operators

Job North Shore
Source No 1105 Bellitzer, St. A

Operators DVA & T.F.
Meter Box No. 15 ΔH@ 1.85 in WC
Gas meter Coeff. 1.0015

Nozzle No. 1-4
Nozzle Dia. 2.77 in.
Bar. Press. 24.38 in.Hg

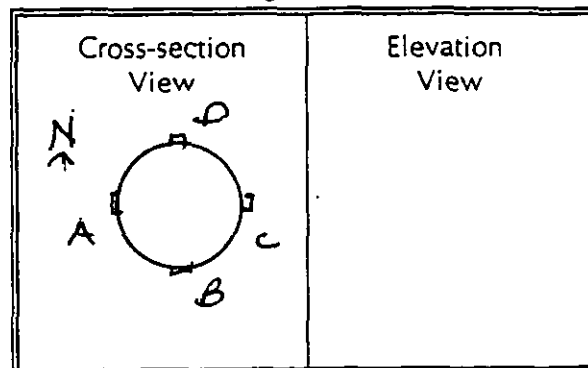
Pilot No. ✓3676
 C_p .84
 H_2O 14.5

[illegible]

INTERPOL LABORATORIES, INC.
(612) 786-6020
EPA Method 2 Field Data Sheet

Drawing of Test Site

Job CYPRUS SILVER BAY
Source 1104 FERTILIZER STACK
Test 3 Run Date 1-10-95
Stack Dimen. 71 IN.
Dry Bulb °F Wet bulb °F
Manometer ☒ Reg. ☐ Exp ☐ Elec.
Barometric Pressure 29.38 IN.HG
Static Pressure -.14 IN.WC
Operators GH SF
Pitot No. 24 V 2.5 C .89
pm



Traverse Point No.	Fraction of Diameter	Distance From Stack Wall (IN.)	Distance From End of Port (IN.)	Velocity	Temp. of Gas (°F)
		Port Length:	IN. <u>5</u>	Time Start: <u>0750</u>	HRS
A 1	.021	1.49	6.49	.42	126
2	.067	4.76	9.76	.59	
3	.118	8.38	13.38	.82	
4	.177	12.57	17.57	.95	
5	.250	17.75	22.75	1.2	
6	.356	25.24	30.25	1.2	
B 1				.45	127
2				.86	
3				1.2	
4				1.2	
5				1.2	
6				1.3	126
C 1				.68	
2				.80	
3				.85	
4				1.2	
5				1.1	
6				1.1	
D 1				.49	126
2				.51	
3				.82	
4				.72	
5				.72	
6				.70	
Temp. Meas. Device & S/N:				<u>0800</u>	Time End: HRS

R or nothing = reg. manometer; S = expanded; E = electronic

032594-G:STACKWP\FORMS\S-392.1

INTERPOL LABORATORIES, INC.

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Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job CYPRUS SILVER BAY Date 1-10-94 Test 3 Run 1
 Source 1104 PEUTZER STACK No. of traverse points 24
 Method _____ Filter holder: GLASS Filter type: 4" GA

Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 IN.HG (vac) ☒Post test: 00 cfm at 10 IN. HG (vac) ☒

Particulate Catch Data:

No. of filters used:

Recovery solvent(s)

7048☐ acetone _____☐ other(s) _____

No. of probe wash bottles:

Sample recovered by:

CH

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2			
Impinger No. 3	<u>670</u>	<u>498</u>	<u>172</u>
Condenser			
Desiccant	<u>1370</u>	<u>1350</u>	<u>20</u>
Total			<u>192</u>

Integrated Gas Sampling Data:

Bag Pump No. 36B
 Bag Material: 5-layer Aluminized Tedlar
 Pretest leak check: 00
 Time start: 0830
 Sampling rate: 400

Box No. 22 Bag No. 1
 Size: 44 L
 cc/min at 23 IN.HG
 (HRS) Time end: 0935 (HRS)
 cc/min Operator: CH

S/N of O₂ Analyzer used to monitor train outlet:36B

052394-G:\STACK\WP\FORMS\SS-0046RR

(612) 786-6020

EPA Method 5 Field Data Sheet

Job CYPRESS SILVER BAYOperator CH SRMeter Box No. 17 ΔH @ 1.73 in. WCNozzle No. 350Nozzle Dia. 1.5 in.Pilot No. 3414C_p .84H₂O 15 %

Date

1-10-95 Test 3 Run 1Gas meter Coeff. .9932Bar. Press. 29.38 in. HgOven 340Imp. 39Gas/In 70Gas/Out 70Oxygen (% v/v) 17.2

Date		104		155		Test		3		Run		1		Gasmeter Coeff.		9932		Bar. Press.		48.0	
Traverse Point No.	Sampling Time (min)	Sample Vol. (cf)	Velocity Head (in. WC)	Orifice Meter (in. WC)	Des. Vol. (cf)	VAC. (in. Hg)	Temperatures (°F)					Oxygen (% v/v)									
							Stack	Probe	Oven	Imp.	Gas/In		Gas/Out								
A	0830	932.800																			
	3.5	935.43	1.2	3.30	5.42	6	126	239	340	39	70	70	17.2								
	5	938.04	1.2	3.38	8.04	6	128				72	70	17.3								
	7.5	940.49	1.0	2.75	0.45	5	129				73	70	17.3								
	10	942.73	.88	2.43	2.70	5	129	240	241	41	74	70	17.2								
B	12.5	944.56	.60	1.62	4.57	5	132				78	72	17.0								
	15	946.29	.49	1.35	6.36	5	132				78	72	17.2								
	17.5	948.86	1.2	3.31	8.91	7	132	246	263	42	79	72	17.1								
	20	951.49	1.3	3.39	1.66	7	132				80	72	17.4								
	22.5	954.31	1.2	3.31	4.30	7	132	249	251	44	85	73	17.4								
C	25	956.65	1.0	2.74	6.73	6	132				85	73	17.3								
	27.5	958.99	.85	2.36	8.98	6	132				85	73	17.3								
	30	960.54	.44	1.22	0.60	6	132	251	260	45	86	73	17.4								
	32.5	963.17	1.1	3.06	3.15	6	132				86	74	17.4								
	35	965.59	1.1	3.01	5.70	6	132				86	74	17.4								
D	37.5	968.10	1.0	2.74	8.14	6	131				87	74	17.4								
	40	970.39	.89	2.44	0.44	6	133	253	264	41	87	75	17.4								
	42.5	972.40	.65	1.81	2.41	5	133				87	75	17.4								
	45	974.05	.45	1.26	4.05	5	133				89	75	17.5								
	47.5	976.21	.79	2.24	6.22	5	133	254	266	42	89	75	17.5								
E	50	978.19	.70	1.96	8.27	5	133				89	75	17.5								
	52.5	980.36	.69	1.93	0.30	5	132				90	75	17.5								
	55	982.44	.75	2.10	2.43	5	132	255	267	43	90	76	17.6								
	57.5	984.31	.64	1.79	4.31	5	133				90	76	17.6								
	60	986.12	.52	1.46	6.14	5	133	257	268	44	90	76	17.6								
	0935																				
	0-60	V _a - 53.32		2.39 ΔH																	

INTERPOLL LABORATORIES, INC.

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Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job CYPRUS SILVER BAY Date 1-10-95 Test 3 Run 2
 Source 1104 PELLETIZER STACK No. of traverse points 24
 Method _____ Filter holder: GLASS Filter type: 4" GF

Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 IN.HG (vac) ☒
 Post test: .00 cfm at 10 IN. HG (vac) ☒

Particulate Catch Data:

No. of filters used:

Recovery solvent(s)

☒ Acetone _____☐ other(s) _____

No. of probe wash bottles:

Sample recovered by:

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2			
Impinger No. 3	684	497	186
Condenser			
Desiccant	1362	1346	16
Total			202

Integrated Gas Sampling Data:

Bag Pump No. 360 Box No. 32 Bag No. 2
 Bag Material: 5-layer Aluminized Tedlar Size: 44 L
 Pretest leak check: .00 cc/min at 23 IN.HG
 Time start: 1005 (HRS) Time end: 1155 (HRS)
 Sampling rate: 400 cc/min Operator: GH

S/N of O₂ Analyzer used to monitor train outlet: 360

052394-G:STACKWPAFORM5S-0046RR

Job Source: CYPRUS SWER BAY
 Date: 1-10-95 Test Run: 2
 Operators: GH SF
 Meter Box No.: 17 $\Delta H @ 1.73$ in.WC
 Gas meter Coeff.: .9933
 Nozzle No.: 1350
 Nozzle Dia.: 1-4 in.
 Bar. Press.: 29.38 in.Hg
 Pilot No.: 27025
 C_p: 84
 H₂O: 15 %

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EPA Method 5 Field Data Sheet

Traverse Point No.	Sampling Time (min)	Sample Vol. (cf)	Velocity Head (in. WC)	Orifice Meter (in. WC)	Des. Vol. (cf)	VAC. (in. Hg)	Temperatures (°F)					Oxygen (% v/v)	
							Stack	Probe	Oven	Imp.	Gas/In		Gas/Out
D	100.5	986.40		2.00	940	5	130	262	249	39	80	75	17.4
	35	988.45	.72	2.00	0.55	5	130				81	75	17.4
	5	990.03	.74	2.06	2.62	5	130				82	75	17.4
	7.5	992.58	.72	2.01	4.66	5	131	263	251	40	83	75	17.3
	10	994.60	.70	1.95	6.63	5	131				81	76	17.3
C	13.5	996.61	.65	1.82	8.44	5	131				82	76	17.4
	15	998.45	.55	1.53	0.99	7	131	264	255	42	82	76	17.6
	17.5	1000.98	1.1	3.06	2.65	7	131				87	76	17.5
	20	1003.61	1.2	3.34	6.10	7	131	26			88	77	17.5
	22.5	1006.10	1.0	2.80	8.40	7	130	266	258	43	89	76	17.5
B	25	1008.40	.88	2.47	0.44	5	132				89	76	17.6
	27.5	1010.41	.69	1.93	3.15	5	132				90	76	17.5
	30	1012.15	.49	1.37	4.83	7	132	267	259	44	89	77	17.5
	32.5	1014.79	1.2	3.36	7.52	7	131				90	77	17.5
	35	1017.55	1.2	3.36	9.97	7	131				90	77	17.5
	37.5	1019.97	1.0	2.81	2.42	7	132	266	255	40	91	78	17.5
	40	1022.42	1.0	2.80	4.74	7	132				91	77	17.5
	42.5	1024.79	.89	2.50	6.47	7	132				91	77	17.4
	45	1026.47	.49	1.38	9.13	8	132	267	256	41	91	77	17.4
	47.5	1029.15	1.2	3.36	1.84	8	132				92	78	17.5
A	50	1031.94	1.2	3.36	4.69	8	132				92	78	17.5
	52.5	1034.28	1.0	2.81	6.65	8	132	269	258	42	92	78	17.7
	55	1036.66	.92	2.58	8.65	8	133	269	258	42	92	78	17.7
	57.5	1038.69	.66	1.85	0.31	7	133				92	78	17.7
	60	1040.31	.45	1.24	0.31	7	133				92	78	17.7
(1155)													
		V _m - 53.94		2.41							Avg. -	82.2	
		0 - 60											

INTERPOLL LABORATORIES, INC.

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Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job CYPRUS SILVER BAY Date 12-10-95 Test 3 Run 3Source 1104 PELLITIZER STACK No. of traverse points 24Method Filter holder: GLASS Filter type: 4" GF

Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 IN.HG (vac) ☒Post test: 00 cfm at 10 IN. HG (vac) ☒

Particulate Catch Data:

No. of filters used:

Recovery solvent(s)

☒ Acetone ☐ other(s)

No. of probe wash bottles:

1

Sample recovered by:

GH

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2			
Impinger No. 3	672	492	180
Condenser			
Desiccant	1385	1370	15
Total			195

Integrated Gas Sampling Data:

Bag Pump No. 36BBox No. 22 Bag No. 3Bag Material: 5-layer Aluminized TedlarSize: 44 LPretest leak check: 00cc/min at 23 IN.HGTime start: 400(HRS) Time end: (HRS)Sampling rate: 400cc/min Operator: GHS/N of O₂ Analyzer used to monitor train outlet: 36B

052394-G:ASTACK\WP\FORMS\SS-0046RR

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EPA Method 5 Field Data Sheet

Job CYPRUS SILVER BAY Operators CH SF Nozzle No. 1-14 Pilot No. 2413.5
 Source 1104 FEMILIZER Meter Box No. 17 ΔH @ 1.73 in. WC Nozzle Dia. 2.850 in. C_p 1.87
 Date 1-10-95 Test 3 Run 3 Gas Meter Coeff. 0.9932 Bar. Press. 29.38 in. Hg H_2O 15 %

Traverse Point No.	Sampling Time (min)	Sample Vol. (cf)	Velocity Head (in. WC)	Orifice Meter (in. WC)	Des. Vol. (cf)	VAC. (in. Hg)	Temperatures (°F)					Oxygen (% v/v)	
							Stack	Probe	Oven	Imp.	Gas/in		Gas/Out
A	(1726)	40.600											
	6 2.5	43.16	1.1	308	3.16	7	130	246	257	39	80	77	17.3
	5 5	45.72	1.1	5.71	3.06	7	131				86	77	17.3
	4 7.5	48.19	1.0	2.83	2.17	7	135				86	77	17.3
	3 10	50.59	.95	2.68	0.56	5	127	261	263	49	89	77	17.4
B	2 12.5	52.51	.60	1.70	2.47	5	127				90	77	17.5
	1 15	54.13	.45	1.27	4.13	5	128				91	77	17.4
	6 17.5	56.85	1.2	3.38	6.82	7	129	263	265	49	91	77	17.4
	5 20	59.69	1.3	3.66	9.62	7	129				91	77	17.5
	4 22.5	62.11	1.0	2.81	2.08	7	130	264	269	51	91	77	17.4
C	3 25	64.49	.96	2.70	4.48	7	130				92	78	17.5
	2 27.5	66.78	.87	2.56	6.74	5	132	264	269	51	92	78	17.4
	1 30	68.49	.50	1.41	8.48	5	133				92	78	17.5
	6 32.5	71.89	1.1	3.08	18.0	7	133	266	271	55	92	78	17.4
	5 35	73.51	1.0	2.80	3.51	7	133				92	78	17.4
D	4 37.5	75.96	1.0	2.81	5.97	7	133				92	78	17.4
	3 40	78.42	1.0	2.81	8.43	7	131	261	269	51	92	78	17.5
	2 42.5	80.77	.90	2.53	0.76	7	133				92	78	12.5
	1 45	82.84	.70	1.97	2.82	7	132	262	271	52	92	78	12.6
	6 47.5	87.91	.75	2.11	4.95	7	132				92	78	12.6
	5 50	87.02	.70	1.97	7.01	7	132				92	78	12.6
	4 52.5	89.18	.74	2.09	9.13	5	131				93	78	12.6
	3 55	91.21	.70	1.91	1.20	5	131	261	264	55	93	78	12.5
	2 57.5	93.06	.51	1.61	3.06	5	131				93	78	12.4
	1 60	94.85	.45	1.27	4.72	5	131				93	78	12.5
	(1330)												
	0 -	V _a - 5425		ΔH _L							Avg.	84.1	

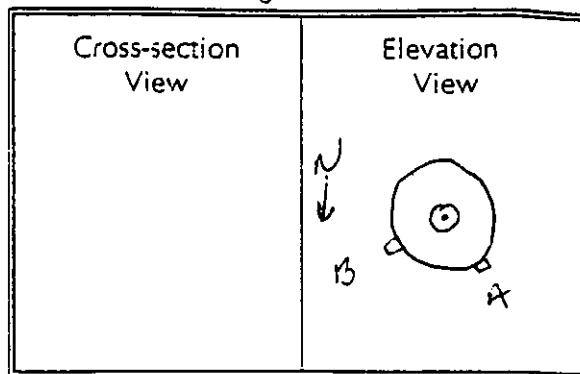
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EPA Method 2 Field Data Sheet

Drawing of Test Site

Job Cypress Northshore
 Source MS 1205 Waste gas
 Test 4 Run Date 1/11/93
 Stack Dimen. 71.5 IN.
 Dry Bulb °F Wet bulb °F
 Manometer ☒ Reg. ☐ Exp ☐ Elec.
 Barometric Pressure 29.62 IN.HG
 Static Pressure -0.3 IN.WC
 Operators J.S. DRH TF
 Pitot No. 1123-10 C₂ .84



Traverse Point No.	Fraction of Diameter	Distance From Stack Wall (IN.)	Distance From End of Port (IN.)	Velocity	Temp. of Gas (°F)
		Port Length: <u>45</u> IN.		Time Start:	HRS
A 1	.021	1.50	6.0		
2	.067	4.79	9.29		
3	.118	8.44	12.73		
4	.177	12.66	17.16		
5	.25	17.88	22.38		
6	.356	25.45	29.95		
7	.644	46.05	50.55		
8	.75	53.62	58.12		
9	.823	58.84	63.34		
10	.882	63.06	67.56		
11	.933	66.71	71.21		
12	.979	69.99	74.50		
B 1					
2					
3					
4					
5					
6					
7					
8					
9					
10					
11					
12					

Temp. Meas. Device & S/N:

Time End:

HRS

R or nothing = reg. manometer; S = expanded; E = electronic

032594-GASTACK\WP\FORMS\S-392.

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job NORTH Shore Date 1/11/ Test 4 Run 1
Source NO 1205 WASTE GAS STATION No. of traverse points 24
Method 572 Filter holder: 9/655 Filter type: glass fiber

Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 IN.HG (vac) ☒
Post test: 0 cfm at 12 IN. HG (vac) ☒

Particulate Catch Data:

No. of filters used:

Recovery solvent(s)

7065

☒ acetone
☐ other(s)

No. of probe wash bottles:

Sample recovered by:

1
DUT

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2	<u>619</u>	<u>498</u>	<u>121</u>
Impinger No. 3	<u>373</u>	<u>366</u>	<u>6</u>
Condenser			
Desiccant			<u>21</u>
Total			<u>148</u>

Integrated Gas Sampling Data:

Bag Pump No. 36A Box No. 28 Bag No. 1
Bag Material: 5-layer Aluminized Tedlar Size: 44 L
Pretest leak check: 0 cc/min at 14 IN.HG
Time start: 5:40 (HRS) Time end: 9:40 (HRS)
Sampling rate: 400 cc/min Operator: DUT

S/N of O₂ Analyzer used to monitor train outlet: 36A

052394-G:STACK\WP\FORMS\SS-0046RR

INTERPOLL LABORATORIES, INC.

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Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job North Shore Date 1/11/95 Test 4 Run 2
 Source N. 1205 West gas No. of traverse points 24
 Method 5+6 Filter holder: glass Filter type: glass fiber

Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 IN.HG (vac) ☒Post test: 0 cfm at 11 IN. HG (vac) ☒

Particulate Catch Data:

No. of filters used:

Recovery solvent(s)

☒ acetone☐ other(s)

No. of probe wash bottles:

Sample recovered by:

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2	690	493	197
Impinger No. 3	390	385	5
Condenser			
Desiccant	1418	1401	17
Total			219

Integrated Gas Sampling Data:

Bag Pump No. 36A Box No. 28 Bag No. 2
 Bag Material: 5-layer Aluminized Tedlar Size: 44 L
 Pretest leak check: 0 cc/min at 15 IN.HG
 Time start: 10:22 (HRS) Time end: 11:25 (HRS)
 Sampling rate: 400 cc/min Operator: J.S

S/N of O₂ Analyzer used to monitor train outlet:36A

052394-G:\STACK\WP\FORMS\S-0046RR

EPA Method 5 Field Data Sheet

Job Cypress Northshore
 Source W356 405
 Date 1/11/95 Test 4 Run 32

Operators QUH + J.F. J.S.
 Meter Box No. 15 $\Delta H @$ 1.85 in. WC
 Gas meter Coeff. 1.0015

Nozzle No. 7-4
 Nozzle Dia. 12.41 in.
 Bar. Press. 27.03 in. Hg

Pilot No. U25-6
 C_p 8.1
 H_2O 15 %

Traverse Point No.	Sampling Time (min)	Sample Vol. (cf)	Velocity Head (in. WC)	Orifice Meter (in. WC)	Des. Vol. (cf)	VAC. (in. Hg)	Temperatures (°F)					Oxygen (% v/v)	
							Stack	Probe	Oven	Imp.	Gas/In		Gas/Out
	10:32	32.60											
A 12	2.5	34.55	.60	1.67	34.40	6	137	230				74	20.1
11	5	36.34	.63	1.76	36.27	6	137		273	34		74 73	19.7
10	7.5	36.19	.61	1.91	38.20	6	144					74 73	20.6
9	10	40.13	.77	2.15	40.26	7	141	232	268	36	83	73	20.0
8	12.5	42.17	.83	2.32	42.41	8	142				85	73	20.0
7	15	44.26	.81	2.29	44.54	8	137				88	73	20.2
6	17.5	46.32	.77	2.18	46.62	8	138	239	275	43	89	73	20.4
5	20	48.40	.84	2.37	48.79	8	139				89	74	20.5
4	22.5	50.55	.84	2.39	50.96	8	140				90	75	20.5
3	25	52.63	.78	2.19	53.06	8	143	246	273	45	90	75	20.6
2	27.5	54.90	.66	1.86	54.98	9	142				91	76	20.8
1	30	56.83	.55	1.56	56.75	8	140	236	258	50	91	76	18.4
B 12	32.5	58.92	.76	2.21	58.85	7	140				90	76	18.4
11	35	60.98	.75	2.13	60.92	8	138				90	77	18.5
10	37.5	62.90	.82	2.12	62.98	8	141				90	77	18.5
9	40	64.93	.84	2.31	65.13	8	142	229	268	41	91	78	18.5
8	42.5	67.12	.89	2.52	67.37	9	141				91	78	18.6
7	45	69.32	.91	2.59	69.65	10	138				91	78	18.7
6	47.5	71.61	.88	2.50	71.89	10	138	248	264	43	90	79	18.7
5	50	73.89	.86	2.51	74.13	10	137				90	79	18.6
4	52.5	76.19	.81	2.31	76.28	11	137				90	79	18.7
3	55	78.32	.67	1.90	78.23	8	140	245	269	51	89	79	18.9
2	57.5	80.18	.59	1.67	80.06	6	142				89	79	18.9
1	60	81.81	.51	1.53	81.81	5	142				89	79	18.9
	11:25												
	0 -	V _m - 49.21		2.12								AVE. - 8.9	

INTERPOLL LABORATORIES, INC.
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Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job North Shore Date 1/11/8 Test 4 Run 3
Source NO 1205 Waste Gas Stack No. of traverse points 24
Method 5 Filter holder: glass Filter type: glass fiber

Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 IN.HG (vac) ☒

Post test: 0 cfm at 13 IN. HG (vac) ☒

Particulate Catch Data:

No. of filters used:

Recovery solvent(s)

☒ acetone

☐ other(s)

No. of probe wash bottles:

Sample recovered by:

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2	687	200 ⁴⁹⁴	193
Impinger No. 3	417	401	16
Condenser			
Desiccant	1378	1364	14
Total			223

Integrated Gas Sampling Data:

Bag Pump No. 36A Box No. 28 Bag No. 3
Bag Material: 5-layer Aluminized Tedlar Size: 44 L
Pretest leak check: 0 cc/min at 14 IN.HG
Time start: 11:53 (HRS) Time end: 12:53 (HRS)
Sampling rate: 400 cc/min Operator: DJA

S/N of O₂ Analyzer used to monitor train outlet:

36A

052394-G:\STACK\WP\FORMS\S-0046RR

EPA Method 5 Field Data Sheet

Job Source Northshore Waste Stacks Date 11/19/95 Test 4 Run 3

Operators QUH, T.F. J.S. Meter Box No. 15 ΔH @ 1.85 in. WC Gasmeter Coeff. 1.0015

Nozzle No. 7-9 Nozzle Dia. 2.17 in. Bar. Press. 24.02 in. Hg

Pilot No. U23-10 C_p 1.84 H_2O 17 %

Date		Run		Test		Gasmeter Coeff.		Sample Vol. (cf)	Velocity Head (in. WC)	Orifice Meter (in. WC)	Des. Vol. (cf)	VAC. (in. Hg)	Temperatures (°F)				Oxygen (% v/v)	
Traverse Point No.	Sampling Time (min)					Stack	Probe						Oven	Imp.	Gas/In	Gas/Out		
	11:53		82.20															
12	2.5		83.78		.70	1.92	84.15	6			135	260	272	40	87	79		19.0
11	5		85.66		.69	1.89	86.16	6.5			135				89	79		19.1
10	7.5		87.67		.74	2.05	88.13	7.5			137				90	79		19.1
9	10		89.74		.81	2.20	90.23	8			143	257	234	41	91	79		19.1
8	12.5		91.85		.89	2.41	92.42	8.5			145				92	79		19.2
7	15		94.11		.92	2.52	94.67	9.5			139	251			93	79		19.4
6	17.5		96.36		.88	2.37	96.85	10			136	251	246	43	93	80		19.4
5	20		98.62		.81	2.39	99.04	10			137				93	80		19.5
4	22.5		100.92		.79	2.17	101.13	10			137				93	80		19.1
3	25		103.11		.67	1.94	103.06	9			138	259	260	45	94	80		19.2
2	27.5		105.20		.59	1.61	104.86	9			141				94	81		19.2
1	30		106.73		.50	1.38	106.54	9			136				94	81		19.2
12	32.5		108.26		.60	1.65	108.36	9			138	263	272	48	94	81		19.3
11	35		109.84		.58	1.60	110.16	9			138				94	79		19.3
10	37.5		111.63		.67	1.81	112.01	6			145				96	82		19.0
9	40		113.58		.75	2.05	114.10	7.5			145	261	278	41	96	82		19.1
8	42.5		115.61		.87	2.65	116.17	7			149				96	80		19.3
7	45		117.59		.86	2.44	120.3	8			139				96	81		19.3
6	47.5		119.57		.91	2.44	120.3	8			139	258	265	44	96	75		19.5
5	50		121.59		.76	2.09	122.44	4			139				94	80		19.6
4	52.5		123.68		.69	1.89	124.46	8.5			139				94	80		19.7
3	55		125.79		.61	1.70	126.25	9			139	267	271	54	94	81		19.6
2	57.5		127.92		.59	1.62	128.06	9			141				94	81		19.6
1	60		130.02		.56	1.53	129.82	9			140				94	81		19.6
	12:53																	
	0 -					1.97 ΔH										AVG. - 86.7		
			$V_s = 477.82$															

Interpoll Laboratories
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EPA Method 7 Sample Collection
Field Data Sheet

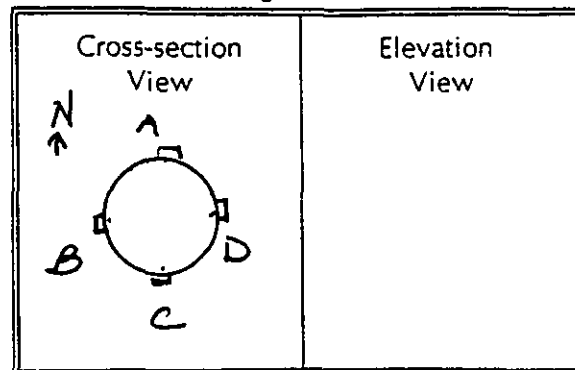
Job Cyprus NORTH Shore Date 1/11/85 Bar. Pressure 29.02 IN.HG.
Test Location DUN, J.B. Fuel Type Sample Train No. 1
NO 1205 WASTE GAS Stack Technician DUN + J.B. Pump No. 23-3
+ J.S.

No.	Test Run Point	Flask No.	Time (HRS)	Vacuum (IN.HG.)	Flask Temp. (°F)	Leak Rate < 0.4 IN.HG./MIN.
1	4/1/1	1	0851	26.1	70	☒ Yes ☐ No
2	4/1/2	2	0900	26.2	71	☒ Yes ☐ No
3	4/1/3	3	0920	26.2	68	☒ Yes ☐ No
4	4/1/1	4	0941	26.4	71	☒ Yes ☐ No
5	4/2/2	5	1041	26.4	69	☒ Yes ☐ No
6	4/2/3	6	1050	26.4	71	☒ Yes ☐ No
7	4/2/1	7	1105	26.2	70	☒ Yes ☐ No
8	4/2/2	9	1120	26.3	69	☒ Yes ☐ No
9	4/3/3	10	1202	26.4	69	☒ Yes ☐ No
10	4/3/1	11	1214	26.3	70	☒ Yes ☐ No
11	4/3/2	12	1230	26.3	70	☒ Yes ☐ No
12	4/3/3	18	1242	26.3	69	☒ Yes ☐ No
13	BLANK	13				☐ Yes ☐ No
14						☐ Yes ☐ No
15						☐ Yes ☐ No
16						☐ Yes ☐ No
17						☐ Yes ☐ No
18						☐ Yes ☐ No
19						☐ Yes ☐ No
20						☐ Yes ☐ No
21						☐ Yes ☐ No
22						☐ Yes ☐ No
23						☐ Yes ☐ No
24						☐ Yes ☐ No
25						☐ Yes ☐ No
26						☐ Yes ☐ No
27						☐ Yes ☐ No

EPA Method 2 Field Data Sheet

Drawing of Test Site

Job CYPRUS NORTH SHORE
 Source 1204 WASTE GAS STACK
 Test 5 Run Date 1-11-95
 Stack Dimen. 71.5 IN.
 Dry Bulb °F Wet bulb °F
 Manometer ☒ Reg. ☐ Exp ☐ Elec.
 Barometric Pressure 29.02 IN.HG
 Static Pressure + .26 IN.WC
 Operators GA SP
 Pitot No. 2412.5 C_p .84
JM



Traverse Point No.	Fraction of Diameter	Distance From Stack Wall (IN.)	Distance From End of Port (IN.)	Velocity	Temp. of Gas (°F)
		Port Length: <u>5</u> IN.	Time Start: <u>0745</u> HRS		
A 1	.021	1.5	6.5	.58	136
2	.067	4.79	9.79	.71	
3	.118	8.44	13.44	.79	
4	.177	12.66	17.66	.91	
5	.250	17.87	22.87	.96	
6	.356	25.45	30.45	.98	
B 1				.50	136
2				.61	
3				.61	
4				.72	
5				.84	
6				.91	
C 1				.55	136
2				.61	
3				.73	
4				.87	
5				.89	
6				.93	
D 1				.71	
2				.78	136
3				.76	
4				.94	
5				.94	
6				.91	
Temp. Meas. Device & S/N: <u>POT 25</u>				<u>0755</u> Time End:	HRS

R or nothing = reg. manometer; S = expanded; E = electronic

INTERPOLL LABORATORIES, INC.

(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job CYPRUS N SHOREDate 1-11-94 Test 5 Run 1Source 1204 WASTE GASNo. of traverse points 24Method 5 Filter holder: GLASSFilter type: 4" GF

Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 IN.HG (vac) ☒Post test: 0.16 cfm at 5 IN. HG (vac) ☒

Particulate Catch Data:

No. of filters used:

Recovery solvent(s)

☒ Acetone _____☐ other(s) _____

No. of probe wash bottles:

Sample recovered by:

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2			
Impinger No. 3	<u>704</u>	<u>499</u>	<u>205</u>
Condenser			
Desiccant	<u>1395</u>	<u>1362</u>	<u>13</u>
Total			<u>218</u>

Integrated Gas Sampling Data:

Bag Pump No. 36BBox No. 19Bag No. 1Bag Material: 5-layer Aluminized TedlarSize: 44 LPretest leak check: 20

cc/min at

23 IN.HGTime start: 0840(HRS) Time end: 0942

(HRS)

Sampling rate: 100cc/min Operator: GHS/N of O₂ Analyzer used to monitor train outlet: 36B

052394-G:\STACK\WP\FORMS\5-0046RR

2 EPA Method 5 Field Data Sheet

Job CIPRUS A. SAKRE
 Source 1204 WASTE GAS STACK
 Date 1-11-95 Test 5 Run 1

Operators GH SF
 Meter Box No. 174H in WC
 Gas meter Coeff. 0.953

Nozzle No. 1-4
 Nozzle Dia. 0.350 in.
 Bar. Press. 29.02 in. Hg

Pilot No. 24020
 C_p 89
 H₂O 18 %

Traverse Point No.	Sampling Time (min)	Sample Vol. (cf)	Velocity Head (in. WC)	Orifice Meter (in. WC)	Des. Vol. (cf)	VAC. (in. Hg)	Temperatures (°F)					Oxygen (% v/v)	
							Stack	Probe	Oven	Imp.	Gas/In		Gas/Out
A	0840	106.200											
	2.5	108.42	.95	2.40	8.43	5	136	249	260	39	40	39	17.5
	5	110.50	.96	2.32	0.58	5	137	247	259	41	59	53	17.2
	7.5	112.58	.90	2.25	2.74	5	137	250	261	45	62	54	17.7
	10	114.55	.80	2.00	4.78	5	139	250	261	49	65	55	17.7
B	12.5	116.68	.70	1.76	6.63	5	139	251	263	49	67	56	17.7
	15	118.30	.57	1.44	8.43	5	139	250	263	49	67	56	17.3
	17.5	120.49	.95	2.39	0.66	5	139	251	263	47	68	57	17.3
	20	122.70	.88	2.25	2.82	5	139	254	264	48	71	57	17.3
	22.5	124.60	.72	1.82	4.77	5	141	258	269	50	73	57	17.3
C	25	126.59	.65	1.64	6.63	5	141	254	269	50	73	59	17.3
	27.5	128.40	.60	1.59	8.42	5	140	255	259	48	74	60	17.3
	30	130.00	.48	1.21	0.02	5	146	257	260	47	75	60	17.3
	32.5	132.28	.90	2.27	7.21	5	146	261	263	49	75	60	17.3
	35	134.39	.85	2.18	4.35	5	136	247	263	47	76	61	17.3
D	37.5	136.35	.70	1.79	6.30	5	138	250	264	46	76	62	17.2
	40	138.19	.64	1.62	8.16	5	139	257	264	47	77	62	17.7
	42.5	139.89	.53	1.40	9.80	5	144	254	269	46	77	63	17.7
	45	141.52	.50	1.26	1.52	5	151	258	271	47	77	63	17.7
	47.5	143.77	.95	2.38	3.76	5	151	259	281	46	76	64	17.4
	50	146.09	.94	2.40	6.02	5	140	260	270	40	79	65	17.4
	52.5	148.21	.83	2.19	8.18	5	137	261	265	40	80	66	17.3
	55	150.28	.78	2.01	0.25	5	137	264	259	42	80	66	17.3
	57.5	152.27	.70	1.94	2.01	5	137	266	260	43	81	66	17.3
	60	154.18	.65	1.68	4.18	5	137	267	265	44	81	66	17.3
(0942)													
	0-60	V _m = 47.98		1.92							AVG. = 65.7		

INTERPOLL LABORATORIES, INC.

(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job CYPRUS N SHORE Date 1-19-95 Test 5 Run 2
 Source 1204 WASTE GAS No. of traverse points 24
 Method 5 Filter holder: GLASS Filter type: 4" GF

Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 IN.HG (vac) ☒Post test: 0.00 cfm at 10 IN. HG (vac) ☒

Particulate Catch Data:

No. of filters used:

Recovery solvent(s)

☒ acetone _____☐ other(s) _____No. of probe wash bottles: 6Sample recovered by: CH

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2			
Impinger No. 3	<u>8899</u>	<u>490</u>	<u>209</u>
Condenser			
Desiccant	<u>1344</u>	<u>1354</u>	<u>10</u>
Total			<u>219</u>

Integrated Gas Sampling Data:

Bag Pump No. 36B
 Bag Material: 5-layer Aluminized Tedlar
 Pretest leak check: 0.00
 Time start: 1032
 Sampling rate: 400

Box No. 19 Bag No. 2
 Size: 44 L
 cc/min at 23 IN.HG
 (HRS) Time end: 1126 (HRS)
 cc/min Operator: CH

S/N of O₂ Analyzer used to monitor train outlet: 360

052394-G:\STACK\WP\FORMS\S-0046RR

EPA Method 5 Field Data Sheet

Job CXPRUS N SHORE Operators GA SF Nozzle No. 1-4 Pilot No. 84
 Source 1204 WASTE GAS STACK Meter Box No. 1770 in. WC. Nozzle Dia. 2.50 in. C_p 24.1 $\pm$ 2.0
 Date 1-11-95 Test 5 Run 2 Gasometer Coeff. 0.9432 Bar. Press. 29.02 in. Hg. H_2O 18 %

Traverse Point No.	Sampling Time (min)	Sample Vol. (cf)	Velocity Head (in. WC)	Orifice Meter (in. WC)	Des. Vol. (cf)	VAC. (in. Hg)	Temperatures (°F)					Oxygen (% v/v)	
							Stack	Probe	Oven	Imp.	Gas/In		Gas/Out
	1022	614.54											
A P 6	2.5	156.75	.95	2.35	6.74	5	147	267	234	40	69	67	17.9
	5	158.89	.93	2.38	8.99	5	136	267	238	41	68	73	17.1
	7.5	161.95	.86	2.21	1.15	5	137	268	241	42	68	75	17.1
	10	163.00	.70	1.81	3.12	5	134	270	246	43	68	77	17.1
	12.5	164.91	.59	1.53	4.92	5	136	259	245	43	79	69	17.0
C	15	166.61	.55	1.42	6.67	5	139	260	251	44	80	69	16.9
	17.5	168.79	.84	2.17	8.82	5	139	264	260	45	81	68	17.0
	20	170.80	.75	1.94	0.86	5	138	259	233	46	82	70	17.1
	22.5	172.84	.70	1.82	2.84	5	138	259	236	47	82	70	17.2
	25	174.70	.62	1.61	4.69	5	137	260	235	49	84	70	17.3
B	27.5	176.39	.57	1.39	6.42	5	145	261	237	49	84	70	17.1
	30	178.05	.45	1.13	8.00	5	150	262	240	44	85	71	17.2
	32.5	180.29	.95	2.42	0.28	5	150	262	241	45	82	72	17.2
	35	182.50	.82	2.14	2.42	5	136	266	245	46	85	72	17.2
	37.5	184.43	.70	1.82	4.41	5	137	265	248	47	86	72	17.2
A	40	186.34	.66	1.72	6.34	5	138	265	249	48	87	72	17.0
	42.5	188.19	.59	1.54	8.16	5	140	266	250	46	87	73	17.7
	45	189.90	.50	1.30	9.84	5	143	267	251	42	87	73	17.0
	47.5	192.11	.96	2.50	3.16	5	139	267	252	43	87	74	16.9
	50	194.41	.94	2.46	4.47	5	136	267	255	41	87	74	17.0
	52.5	196.69	.89	2.34	6.72	5	135	265	254	42	87	74	17.0
	55	198.80	.79	2.08	8.84	5	132	266	258	43	88	74	17.0
	57.5	200.94	.75	1.97	0.91	5	135	266	259	44	89	74	17.0
	60	202.735	.60	1.58	2.76	5	136	265	260	44	89	74	17.0
	1126												
	0-60	$V_n - 48.215$		$1.9 \Delta H -$							AVG. -	77.0	

INTERPOLL LABORATORIES, INC.

(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job CYPRUDate 1-11-95 Test 5 Run 3Source 1204 WASTE GASNo. of traverse points 24Method 5 Filter holder: GLASS

Filter type: _____

Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 IN.HG (vac) ☒Post test: .00 cfm at 10 IN. HG (vac) ☒

Particulate Catch Data:

No. of filters used: _____

Recovery solvent(s)

☐ acetone _____☐ other(s) _____

No. of probe wash bottles: _____

Sample recovered by: _____

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2			
Impinger No. 3	<u>700</u>	<u>496</u>	<u>204</u>
Condenser	<u>1360</u>		
Desiccant	<u>1360</u>	<u>1347</u>	<u>13</u>
Total			<u>217</u>

Integrated Gas Sampling Data:

Bag Pump No. 36B

Box No. _____

Bag No. 3Bag Material: 5-layer Aluminized TedlarSize: 44 LPretest leak check: .00

cc/min at

23 IN.HGTime start: 1153(HRS) Time end: 1257

(HRS)

Sampling rate: 400cc/min Operator: GHS/N of O₂ Analyzer used to monitor train outlet: 36B

052394-G:\STACK\WP\FORMS\S-0046RR

EPA Method 5 Field Data Sheet

 Pilot No. 240 U8
 C_g 94
 H₂O 18

 Nozzle No. 1-4
 Nozzle Dia. 250 in.
 Bar. Press. 29.02 in. Hg

 Operators CH SF
 Meter Box No. 17 AH@123 in. WC
 Gas Meter Coeff. 9932

 Job CHARVUS N SHORE
 Source 204 WASTE GAS STACK
 Date 7-11-95 Test 5 Run 3

Date	Time	Test	Run	Gasmeter Coef.	Temperatures (°F)					Oxygen (% v/v)								
					Stack	Probe	Oven	Imp.	Gas/In		Gas/Out							
A	115.3	2.5	203.66	.95	248	530	5	135	246	243	41	76	72	17.3				
								132	245	244	42	78	73	17.3				
								137	246	243	43	81	72	17.1				
								138	248	240	44	81	72	17.0				
								137	251	247	44	82	73	17.0				
								137	249	251	45	84	73	17.0				
								137	243	239	46	84	73	17.1				
								139	245	240	45	84	73	17.1				
								135	238	259	43	84	73	17.0				
								137	235	262	43	85	73	17.1				
B	2.5	224.67	.68	178	468	5	137	233	265	46	85	73	17.1					
							137	239	259	46	86	73	17.1					
							139	241	227	45	86	73	17.1					
							137	244	257	45	86	74	17.2					
							142	251	253	46	87	74	17.3					
							145	257	266	47	87	74	17.3					
							144	260	268	47	88	74	17.3					
							144	261	260	46	88	74	17.3					
							144	257	249	46	88	74	17.3					
							144	252	248	47	88	74	17.3					
C	4.5	243.79	.90	233	979	5	137	251	243	47	88	74	17.3					
							137	251	252	47	88	74	17.3					
							139	257	254	49	89	75	17.3					
							137	263	251	49	89	75	17.3					
															Avg.	79.2		
							0-60	V _a - 49.24	1.97	ΔH -								

Drawing of Test Site

Cross-section View

Elevation View

A

B

N

Traverse Point No.	Fraction of Diameter	Distance From Stack Wall (IN.)	Distance From End of Port (IN.)	Velocity	Temp. of Gas (°F)
		Port Length: 4.5 IN.	Time Start: 0810 HRS		
A	1	.026	1.18	568	72
	2	.082	3.73	823	98
	3	.146	6.64	11.14	1.1
	4	.226	10.38	14.78	1.3
	5	.342	15.56	20.06	1.4
	6	.658	29.94	34.44	1.4
	7	.774	35.22	39.72	1.4
	8	.854	38.86	43.36	1.1
	9	.918	41.77	46.27	.98
	10	.974	44.32	48.87	.74
B	1				.95
	2				.74
	3				.98
	4				1.1
	5				1.3
	6				1.2
	7				1.0
	8				1.0
	9				1.1
	10				.86
					.72
Temp. Meas. Device & S/N: PPT 25				Time End: 0815 HRS	

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Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job CYPRUS N. SHORE Date 1-12-95 Test 6 Run 21
 Source NO 12 FERTILIZER ROTOCONE No. of traverse points 20
 Method 5 Filter holder: GLASS STK Filter type: 4" G.F.

Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 IN.HG (vac) ☒Post test: .00 cfm at 10 IN. HG (vac) ☒

Particulate Catch Data:

No. of filters used:

Recovery solvent(s)

☒ Acetone☐ other(s)

No. of probe wash bottles:

Sample recovered by:

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2			
Impinger No. 3	<u>532</u>	<u>499</u>	<u>33</u>
Condenser			
Desiccant	<u>1370</u>	<u>1360</u>	<u>10</u>
Total			<u>43</u>

Integrated Gas Sampling Data:

Bag Pump No. 36B
 Bag Material: 5-layer Aluminized Tedlar
 Pretest leak check: .00
 Time start: 1005
 Sampling rate: 400 CC

Box No. 16 Bag No. 21
 Size: 44 L
 cc/min at 23 IN.HG
 (HRS) Time end: 1107 (HRS)
 cc/min Operator: GH

S/N of O₂ Analyzer used to monitor train outlet:36B

EPA Method 5 Field Data Sheet

3405 N. SAGE

Operators

Job CITRUS H. STOKS
Source NO 12 ROTACONE STACK NORTH

Date 1-12-95 Test 6 Run.

Gas meter Coeff.

Gas meter Coeff.

64 SF

1.74H@ 1.70 in.WC

1995

19952

Nozzle No.

Nozzle Dia.

Bar. Press. 2

3-

25

517

Pilot No.

U

05

34 ✓

78.

2

Traverse Point No.	Sampling Time (min)	Sample Vol. (cf)	Velocity Head (in. WC)	Orifice Meter (in. WC)	Des. Vol. (cf)	VAC. (in. Hg)	Temperatures (°F)				Gas/In	Gas/Out	Oxygen (% v/v)
							Stack	Probe	Oven	Imp.			
B	0825	253.50			4.8V	2							20.8
10	3	254.89	.74	.61	6.47	2	147	294	229	39	72	71	20.8
9	6	256.48	.93	.82	8.16	2	132	276	231	40	72	71	20.8
8	9	258.17	1.1	.92	0.00	2	134	259	240	40	73	71	20.8
7	12	260.00	1.3	1.09	1.76	3	134	261	240	43	73	71	20.7
6	15	261.76	1.2	1.01	3.60	3	134	262	245	43	74	71	20.7
5	18	263.64	1.3	1.09	5.29	3	134	261	248	44	75	71	20.7
4	21	265.29	1.1	.92	8.50	3	135	262	269	45	75	71	20.7
3	24	268.82	1.0	.84	9.99	3	135	263	257	44	75	71	20.7
2	27	268.47	1.0	.84	1.36	3	135	264	252	45	76	71	20.7
1	30	269.09	.85	.71	2.93	3	135	264	248	45	76	71	20.7
A	33	271.57	1.72	1.60	4.69	3	135	266	248	44	75	71	20.7
9	36	272.94	.94	.79	6.52	3	134	267	259	45	75	71	20.7
8	39	274.70	1.2	1.00	8.43	3	138	268	251	46	76	71	20.7
7	42	276.53	1.3	1.09	0.19	3	138	268	252	47	76	71	20.9
6	45	278.49	1.4	1.17	1.79	3	138	267	250	47	77	72	20.9
5	48	280.54	1.2	1.00	3.58	3	138	268	254	48	77	71	20.9
4	51	281.86	.98	.82	4.86	3	137	269	259	48	77	71	20.9
3	54	283.39	.97	.81	6.10	3	139	259	251	49	77	71	20.9
2	57	284.87	.85	.71		3	139	260	252	49	77	71	20.9
1	60	286.17	.59	.44		3	139	261	253	49	77	71	20.9
	(0926)												
	0-60	V _m = 32.67		.87 ΔH -							AVG. = 73.1		

INTERPOLL LABORATORIES, INC.

(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job CYPRUS N. SHORE Date 1-12-94 Test 6 Run 2Source NO 12 PELLETIZER ROTOCONE No. of traverse points 20Method 5 Filter holder: GLASS STACK Filter type: 4" GF

Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 IN.HG (vac) ☒Post test: 0 cfm at 5 IN. HG (vac) ☒

Particulate Catch Data:

No. of filters used:

Recovery solvent(s)

☒ acetone☐ other(s)

No. of probe wash bottles:

Sample recovered by:

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2			
Impinger No. 3	534	490	44
Condenser			
Desiccant	1319	1312	7
Total			51

Integrated Gas Sampling Data:

Bag Pump No. 36BBag Material: 5-layer Aluminized TedlarPretest leak check: 00Time start: 0925Sampling rate: 400Box No. 16 Bag No. 2Size: 44 Lcc/min at 23 IN.HG(HRS) Time end: 0926 (HRS)cc/min Operator: 64S/N of O₂ Analyzer used to monitor train outlet: 36B

052394-G:\STACK\WP\FORMS\5-0046RR

EPA Method 5 Field Data Sheet

 Pilot No. 246
 C_p 1.81
 H₂O 2 %

 Nozzle No. 1-3
 Nozzle Dia. 1.85 in.
 Bar. Press. 28.94 in. Hg

 Operator's C. S. F.
 Meter Box No. 17AH@1.73 in. WC
 Gas Meter Coeff. 9932

 Job CYPROS N. SPARE
 Source NO. 12 ROTOCONE STACK NORTH
 Date 1-12-95 Test 6 Run 2

Date 1-12-95		Test	Run	Gas Meter Coeff.		Velocity Head (in WC)	Orifice Meter (in WC)	Des. Vol. (cf)	VAC. (in Hg)	Temperatures (°F)					Oxygen (% v/v)	
Traverse Point No.	Sampling Time (min)	Sample Vol. (cf)	Sample Vol. (cf)	Probe	Oven					Imp.	Gas/In	Gas/Out				
A	1005	286.50														
	10	3	288.01	.74	.72	8.00	2	138	244	249	39	72	76		20.9	
	9	6	289.73	.98	.95	9.72	2	136	247	250	40	73	71		20.9	
	8	9	291.64	1.3	1.26	1.69	2	138	249	251	41	73	71		20.9	
	7	12	293.65	1.4	1.36	3.29	2	137	240	246	42	73	71		20.9	
	6	15	295.69	1.3	1.26	5.71	2	140	241	247	42	73	71		20.9	
	5	18	297.62	1.2	1.16	7.61	2	140	242	249	43	77	71		20.9	
	4	21	299.35	1.0	.97	9.34	2	141	243	249	41	77	71		20.9	
	3	24	300.95	.95	.83	0.95	2	139	244	251	42	77	72		20.9	
	2	27	302.47	.75	.73	2.45	2	139	245	258	43	77	72		20.9	
B	1	30	303.91	.70	.68	3.91	2	139	247	252	44	77	72		20.9	
	10	33	305.41	.72	.70	5.39	2	137	249	255	45	77	72		20.9	
	9	36	307.10	.97	.95	7.11	2	136	251	256	45	77	72		20.9	
	8	39	308.86	1.0	.98	8.85	2	137	253	257	45	78	72		20.9	
	7	42	310.90	1.4	1.37	0.92	2	136	253	277	40	78	72		20.9	
	6	45	312.82	1.2	1.18	3.83	2	136	254	255	42	78	72		20.9	
	5	48	314.72	1.2	1.17	4.73	2	140	255	259	43	78	72		20.9	
	4	51	316.72	1.3	1.27	6.72	2	140	255	257	44	78	72		20.9	
	3	54	318.54	1.1	1.07	8.54	2	139	256	257	44	78	72		20.9	
	2	57	320.25	.90	.88	0.26	2	137	257	259	45	78	72		20.9	
1	60	321.90	.85	.83	1.81		137				78	72		20.9		
		(1107)														
0 - 60		V _m = 35.4					1.02								Avg. = 74.0	

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job CYPRUS N SARE Date 1-12-95 Test 6 Run 3Source NO 12 FERTILIZER No. of traverse points 20Method 5 Filter holder: ROTOCONE Filter type: 4" GFSample Train Leak Check: GLASSPretest: ≤ 0.02 cfm at 15 IN.HG (vac) ☒Post test: 100 cfm at 5 IN. HG (vac) ☒

Particulate Catch Data:

No. of filters used: _____

Recovery solvent(s) _____

☒ acetone _____☐ other(s) _____No. of probe wash bottles: 1Sample recovered by: GAH

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2			
Impinger No. 3	1377	1370	7
Condenser			
Desiccant	554	505	49
Total			56

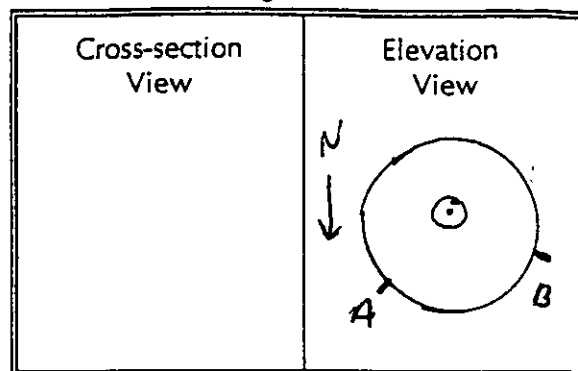
Integrated Gas Sampling Data:

Bag Pump No. 36BBox No. 16 Bag No. 3Bag Material: 5-layer Aluminized TedlarSize: 44 LPretest leak check: .00cc/min at 23 IN.HGTime start: 1136(HRS) Time end: 1322 (HRS)Sampling rate: 400cc/min Operator: GAHS/N of O₂ Analyzer used to monitor train outlet: 36B

EPA Method 2 Field Data Sheet

Drawing of Test Site

Job Cypress Northshore
 Source No. 2 Boiler Stack
 Test 7 Run 1 Date 1/12/95
 Stack Dimen. 110 IN.
 Dry Bulb °F Wet bulb °F
 Manometer ☐ Reg. ☐ Exp ☐ Elec.
 Barometric Pressure 28.94 IN.HG
 Static Pressure -.90 IN.WC
 Operators NUH J.S. TF
 Pitot No. V23-10 C_p .84
PM/SD2



Traverse Point No.	Fraction of Diameter	Distance From Stack Wall (IN.)	Distance From End of Port (IN.)	Velocity	Temp. of Gas (°F)
		Port Length: <u>15</u> IN.		Time Start:	HRS
B 1	.021	2.31	17.31	.80	
2	.067	7.37	22.37	.82	
3	.113	12.98	27.98	.85	
4	.177	19.47	34.47	.83	
5	.250	27.50	42.50	.84	
6	.356	39.16	54.16	.92	
7	.644	76.84	85.84	.99	
8	.750	82.50	97.50	.90	
9	.823	90.53	105.53	.79	
10	.882	97.02	112.02	.78	
11	.933	102.63	117.63	.94	
12	.979	107.69	122.69	.77	
A 1					
2					
3					
4					
5					
6					
7					
8					
9					
10					
11					
12					
Temp. Meas. Device & S/N:				Time End:	HRS

R or nothing = reg. manometer; S = expanded; E = electronic

INTERPOLL LABORATORIES, INC.
(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job Cypress Northshore Date 1/12/95 Test 7 Run 1
Source No. 2 Boiler stack No. of traverse points 24
Method 516 Filter holder: glass Filter type: glass fiber

Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 IN.HG (vac) ☒
Post test: 0 cfm at 15 IN. HG (vac) ☒

Particulate Catch Data:

No. of filters used: _____

Recovery solvent(s)

☒ acetone _____
☐ other(s) _____

No. of probe wash bottles: _____

Sample recovered by: _____

1
DUIT

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2	553	458	55 95
Impinger No. 3	498	489	9
Condenser			
Desiccant	1315	1300	15
Total			119 79

Integrated Gas Sampling Data:

Bag Pump No. 23 B
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check: 0 at
Time start: 9:17
Sampling rate: 400

Box No. 30 Bag No. 1
Size: 44 L
cc/min at 14 IN.HG
(HRS) Time end: 10:17 (HRS)
cc/min Operator: J.S.

S/N of O₂ Analyzer used to monitor train outlet: 4

052394-G:\STACK\WPA\FORMS\S-0046RR

EPA Method 5 Field Data Sheet

Cypress Northshore
Source Northshore
Date 1/12/95 Test 7 Run 1

Operators

Meter Box No. 18 ΔH @ 1.97 in. WCGas meter Coeff. 1.0026

Nozzle No.

Nozzle Dia.

Bar. Press.

Pilot No. 23-10C_p 84H₂O 8in. Hg 28.94

Traverse Point No.	Sampling Time (min)	Sample Vol. (cf)	Velocity Head (in.WC)	Orifice Meter (in.WC)	Des. Vol. (cf)	VAC. (in.Hg)	Temperatures (°F)					Oxygen (% v/v)	
							Stack	Probe	Oven	Imp.	Gas/In		Gas/Out
	(9:17)	123.70											
A 12	25	125.97	1.15	2.65	25.93	9	292	230	252	50	64	59	4.8
11	5	128.15	1.05	2.46	28.12	8	296				66	60	6.0
10	75	130.35	1.20	2.83	30.46	8	296				70	61	4.9
9	10	132.59	1.20	2.83	32.80	8.5	298	233	258	40	72	61	4.6
8	12.5	135.00	1.25	2.95	35.19	9	297				73	62	4.5
7	15	137.23	1.25	2.96	37.60	9.5	296				76	64	4.5
6	17.5	139.62	1.30	3.09	40.06	10	297	235	267	43	76	65	4.5
5	20	142.07	1.35	3.20	42.56	11	300				77	65	4.5
4	22.5	144.54	1.35	2.97	44.97	11	300				78	65	4.7
3	25	146.95	1.10	2.63	47.24	10	296	239	265	39	78	66	4.7
2	27.5	149.23	.93	2.23	49.34	8.5	298				79	66	4.6
1	30	151.37	.95	2.27	51.45	7	298				80	67	4.8
B 12	32.5	153.46	1.06	2.56	53.71	7.5	299	243	256	41	80	68	4.9
11	35	155.62	1.03	2.47	55.92	8	296				83	69	4.6
10	37.5	157.77	1.03	2.48	58.14	8	296				84	69	5.0
9	40	159.91	1.02	2.43	60.34	8	304	241	271	46	85	69	4.8
8	42.5	162.22	1.03	2.46	62.55	8	303				86	70	4.9
7	45	164.49	1.04	2.48	64.77	8	306				87	71	5.0
6	47.5	166.66	1.04	2.48	67.00	8	307	238	274	43	87	71	5.1
5	50	168.94	1.04	2.48	69.22	8.5	309				85	71	4.8
4	52.5	171.26	1.05	2.50	71.45	8.5	309				86	72	5.1
3	55	173.55	1.04	2.48	73.68	8.5	311				89	73	5.1
2	57.5	175.82	1.04	2.49	75.91	9.0	309	233	258	36	90	74	4.7
1	60	177.96	1.01	2.42	78.11	8	309				90	74	5.0
	(10:17)												
	0-60	V _m - 54.26		2.62 ΔH -							Avg. -	73.6	

INTERPOLL LABORATORIES, INC.

(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job Cypress Northshore Date 1/12/95 Test 7 Run 2
 Source No. 2 Boiler Stack No. of traverse points 29
 Method 516 Filter holder: glass Filter type: glass fiber

Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 IN.HG (vac) ☒Post test: 0 cfm at 13 IN. HG (vac) ☒

Particulate Catch Data:

No. of filters used:

Recovery solvent(s)

☒ Acetone☐ other(s)

No. of probe wash bottles:

Sample recovered by:

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2	618	490	128
Impinger No. 3	514	506	8
Condenser	1330	1313	17
Desiccant			
			153
Total			

Integrated Gas Sampling Data:

Bag Pump No.

230

Box No.

30Bag No. 2

Bag Material:

5-layer Aluminized Tedlar

Size:

44 L

Pretest leak check:

0

cc/min at

14

IN.HG

Time start:

~~10:47~~ 10:47

(HRS) Time end:

13:47

(HRS)

Sampling rate:

400

cc/min Operator:

J.S.S/N of O₂ Analyzer used to monitor train outlet:4

052394-GASTACKWP\FORMS\S-0046RR

INTERPOL LABORATORIES, INC.

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EPA Method 5 Field Data Sheet

Operators

Meter Box No. 18

Gasmeter Coeff. 1.0026

Nozzle No. 7-4

Nozzle Dia. 2.47 in.

Bar. Press. 28.14 in. Hg

Pilot No. V 23-10

C_p 34

H₂O 7

Job Cypress

Source Northshore

Date 1/12/95

Test 7

Run 2

Sample Vol. (cc)

Velocity Head (in. WC)

Orifice Meter (in. WC)

Des. Vol. (cc)

VAC. (in. Hg)

Stack

Probe

Oven

Imp.

Gas/In

Gas/Out

Oxygen

Temp. (°F)

AVG. -

86.6

5.0

4.8

4.6

4.7

4.9

4.8

4.7

4.9

4.8

4.6

4.7

4.6

4.5

4.6

4.4

4.4

4.5

4.5

4.5

4.5

4.6

4.7

4.8

4.9

4.7

4.8

4.9

4.7

4.8

4.9

4.7

4.8

4.9

4.7

4.8

4.9

INTERPOLL LABORATORIES, INC.

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Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job Cypress Northshore Date 1/12/95 Test 7 Run 3
 Source No. 2 Boiler Stack No. of traverse points 24
 Method 546 Filter holder: glass Filter type: glass fiber

Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 IN.HG (vac) ☒Post test: 0 cfm at 15 IN. HG (vac) ☒

Particulate Catch Data:

No. of filters used:

Recovery solvent(s)

☒ acetone☐ other(s)

No. of probe wash bottles:

Sample recovered by:

1
Quit

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2	337	200	137
Impinger No. 3			
Condenser			
Desiccant	1315	1329	14
Total			151

Integrated Gas Sampling Data:

Bag Pump No. 230 Box No. 30 Bag No. 3
 Bag Material: 5-layer Aluminized Tedlar Size: 44 L
 Pretest leak check: 0 cc/min at 14 IN.HG
 Time start: 12:17 (HRS) Time end: 13:22 (HRS)
 Sampling rate: 400 cc/min Operator: J.S.

S/N of O₂ Analyzer used to monitor train outlet:4

052394-GASTACKWP\FORMS\S-0046RR

EPA Method 5 Field Data Sheet

Job Cypress Northshore Operators J. S. + D. J. + J. F. Pilot No. U 23-10
 Source Northshore Meter Box No. 16 ΔH₀ 1.81 in. WC Nozzle Dia. 0.25 in.
 Date 1/12/95 Test 7 Run 3 Gas meter Coeff. 1.0026 Bar. Press. 28.74 in. Hg 28.74 in. Hg 6 %

Traverse Point No.	Sampling Time (min)	Sample Vol. (cf)	Velocity Head (in. WC)	Orifice Meter (in. WC)	Des. Vol. (cf)	VAC. (in. Hg)	Temperatures (°F)					Oxygen (% v/v)	
							Stack	Probe	Oven	Imp.	Gas/In		Gas/Out
	12:17	239.60											
A 12	8.5	242.06	1.20	2.96	42.04	9	320	235	258	45	84	79	5.1
11	5	244.48	1.20	2.93	44.46	9	319				87	77	4.7
10	7.8	246.94	1.25	3.05	46.93	9	320				87	78	4.7
9	10	249.37	1.25	3.05	49.40	9	321	242	238	44	88	78	4.6
8	12.5	251.79	1.15	2.81	51.78	9	321				88	78	4.7
7	15	254.28	1.30	3.18	54.31	9.5	320				87	78	4.7
6	17.5	256.69	1.35	3.29	56.87	10	323	248	241	46	88	77	4.7
5	20	259.22	1.30	3.17	59.46	10	321				88	78	4.7
4	22.5	261.78	1.30	3.18	61.92	10.5	321				89	79	4.8
3	25	264.23	1.20	2.93	64.35	10.5	323	245	252	52	89	79	5.0
2	27.5	266.47	1.00	2.45	66.57	8	323				89	79	5.0
1	30	268.53	.67	1.64	68.39	7	322				88	77	5.2
B 12	32.5	270.93	1.30	3.18	70.91	7	320	241	260	45	91	82	5.2
11	35	273.38	1.45	3.56	73.59	11	322				93	82	5.2
10	37.5	276.09	1.50	3.69	76.32	13	322				93	83	4.8
9	40	278.82	1.35	3.33	78.91	13	320	241	263	42	91	83	4.8
8	42.5	281.55	1.45	3.55	81.59	13	324				91	83	4.7
7	45	284.25	1.50	3.68	84.31	13	323				90	83	4.7
6	47.5	286.98	1.55	3.80	87.08	13	323	235	269	44	89	83	4.9
5	50	289.63	1.35	3.32	89.66	12.5	321				89	83	4.9
4	52.5	292.17	1.35	3.32	92.25	12	321				89	83	5.1
3	55	294.81	1.30	3.19	94.78	11	322	238	264	41	89	83	5.2
2	57.5	297.41	1.30	3.26	97.32	11	320				89	82	5.2
1	60	299.86	1.26	2.95	99.76	9	320				90	82	5.2
	13:22												
	0-60	V _m - 60.88		3.14 ΔH ₀							AVG. -	84.7	

Drawing of Test Site

N ↗ Cross-section View 	Elevation View
--	---------------------------

3 - morning; m - reg. manometer; S - expanded; e - electronic

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INTERPOLL LABORATORIES, INC.
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Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job CYPRUS H. SARE Date 1-13-91 Test 8 Run 1
Source NO 2 FINE CRUSHER No. of traverse points 12
Method 5 Filter holder: GLASS Filter type: 4" GF

Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 IN.HG (vac) ☒
Post test: $\leq .02$ cfm at 6 IN. HG (vac) ☒

Particulate Catch Data:

No. of filters used:

Recovery solvent(s)

☒ Acetone _____
☐ other(s) _____

No. of probe wash bottles:

Sample recovered by:

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2			
Impinger No. 3	500	499	1
Condenser			
Desiccant	1340	1325	15
Total			16

Integrated Gas Sampling Data:

AMBIENT

Bag Pump No. _____ Box No. _____ Bag No. _____
Bag Material: 5-layer Aluminized Tedlar Size: 44 L
Pretest leak check: _____ cc/min at _____ IN.HG
Time start: _____ (HRS) Time end: _____ (HRS)
Sampling rate: _____ cc/min Operator: _____

S/N of O₂ Analyzer used to monitor train outlet: _____

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Pilot No.	2466	%
C _p	94	
H ₂ O	2	

EPA Method 5 Field Data Sheet

[illegible]

INTERPOLL LABORATORIES, INC.

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Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job CYRUS N SAORE Date 6-13-94 Test 8 Run 2
Source NO 2 FINE CRUSHER No. of traverse points 12
Method 5 Filter holder: GLASS Filter type: 4" GF

Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 IN.HG (vac) ☒Post test: 0.00 cfm at 7 IN. HG (vac) ☒

Particulate Catch Data:

No. of filters used: _____

Recovery solvent(s)

☐ acetone _____☐ other(s) _____

No. of probe wash bottles: _____

Sample recovered by: _____

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2			
Impinger No. 3	498	497	1
Condenser			
Desiccant	1340	1326	14
			5
Total			15

Integrated Gas Sampling Data:

AMBIENT

Bag Pump No. _____ Box No. _____ Bag No. _____
Bag Material: 5-layer Aluminized Tedlar Size: 44 L
Pretest leak check: _____ cc/min at _____ IN.HG
Time start: _____ (HRS) Time end: _____ (HRS)
Sampling rate: _____ cc/min Operator: _____

S/N of O₂ Analyzer used to monitor train outlet: _____

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EPA Method 5 Field Data Sheet

Job CARUS N. SHORE
Source NO 2 FINE COLLIER
Date 1-13-98 Test 8 Run 2

Operators CH SF
Meter Box No. 17 Δ11@1-7
Gasmeter Coeff. 993

3 in. WC

Nozzle No.
Nozzle Dia.
Bar. Press.

1-4 _____ in.
0250 _____ in.
29202 _____ in. Hg

Pitol No.

$$\begin{array}{r} 2404 \\ .87 \\ 2 \end{array}$$
[illegible]

INTERPOLL LABORATORIES, INC.

(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job CYPRUS N. SHORE Date 1-13-91 Test 8 Run 3
 Source NO 2 FINE CRUSHER No. of traverse points 12
 Method 5 Filter holder: GLASS Filter type: 4" GF

Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 IN.HG (vac) ☒Post test: 2.0 cfm at 7 IN. HG (vac) ☒

Particulate Catch Data:

No. of filters used: _____

Recovery solvent(s) _____

☒ acetone _____☐ other(s) _____

No. of probe wash bottles: _____

Sample recovered by: _____

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2			
Impinger No. 3	493	491	2
Condenser			
Desiccant	1355	1340	15
Total			17

Integrated Gas Sampling Data:

AMBIENT

Bag Pump No. _____
 Bag Material: 5-layer Aluminized Tedlar
 Pretest leak check: _____
 Time start: _____
 Sampling rate: _____

Box No. _____ Bag No. _____
 Size: 44 L
 cc/min at _____ IN.HG
 (HRS) Time end: _____ (HRS)
 cc/min Operator: _____

S/N of O₂ Analyzer used to monitor train outlet: _____

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EPA Method 5 Field Data Sheet

Job OPRUS N SHORE
Source NO 2 FINE CRUSHER
1.12 0.5 1 Run
Operators GH
Meter Box No. 17 ΔH@1.73 in. WC
Gasmeter Coeff. .0032
Nozzle No. 1-4
Nozzle Dia. .250 in.
Bar. Press. 29.02 in. Hg
Pilot No. 2907
 C_p .87
 H_2O 2 %

[illegible]

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Drawing of Test Site

R or nothing - reg. manometer; S - expanded; E - electronic

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Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job Cyprus Northshore Date 1/13/95 Test 9 Run 1
Source Dry Cobble Stack No. of traverse points 12
Method 5 Filter holder: glass Filter type: glass fiber

Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 IN.HG (vac) ☒Post test: 0 cfm at 8 IN. HG (vac) ☒

Particulate Catch Data:

No. of filters used:

Recovery solvent(s)

☒ acetone☐ other(s)

No. of probe wash bottles:

Sample recovered by:

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1	501	503	-2
Impinger No. 2			
Impinger No. 3			
Condenser			
Desiccant	1495	1487	8
Total			6

Integrated Gas Sampling Data:

Ambient air

Bag Pump No. 5
Bag Material: 5-layer Aluminized Tedlar
Pretest leak check: 0
Time start: _____
Sampling rate: _____

Box No. _____ Bag No. _____
Size: 44 L
cc/min at 14 IN.HG
(HRS) Time end: _____ (HRS)
cc/min Operator: _____

S/N of O₂ Analyzer used to monitor train outlet: _____

052394-G:\STACK\WP\FORMS\S-0046RR

EPA Method 5 Field Data Sheet

Job C-1013 Northshore Pilot No. U23-5
 Source Off Color Stack Nozzle No. 3-3
 Date 1/13/95 Test 9 Run 1 Nozzle Dia. 1.82 in. 1.84
 Gas Meter Coeff. 1.0004 Bar. Press. 29.02 in. Hg. 2 %

Traverse Point No.	Sampling Time (min)	Sample Vol. (cf)	Velocity Head (in. WC)	Orifice Meter (in. WC)	Des. Vol. (cf)	VAC. (in. Hg)	Temperatures (°F)					Oxygen (% v/v)	
							Stack	Probe	Oven	Imp.	Gas/In		Gas/Out
	(820)	891.00											
A 12	2.5	892.54	.91	.97	92.41	3	73	293	247	34	65	65	Ambient
11	5	894.02	.90	.97	93.83	3	73				69	69	Air
10	7.5	895.41	.92	.99	95.27	3	73				71	64	
9	10	896.95	.91	.99	96.71	3	71	253	248	37	73	65	
8	12.5	898.43	.95	1.04	98.18	3	71				74	65	
7	15	899.89	.94	1.02	99.65	3	72				74	65	
6	17.5	901.34	.93	1.02	01.11	3	70	266	265	41	74	66	
5	20	902.80	.99	1.08	02.62	3	70				76	65	
4	22.5	904.26	.97	1.09	4.13	3	70				75	67	
3	25	905.69	.94	1.03	5.61	3	69	269	268	42	77	68	
2	27.5	907.18	.97	1.06	7.10	3	74				78	69	
1	30	908.60	.88	.96	8.53	3	74				79	69	
	32.5	910.11	.95	1.04	00.2	3	74	266	271	43	76	69	
11	35	911.59	.98	1.07	1.52	3	74				79	70	
10	37.5	913.01	1.00	1.10	3.04	3	74				79	70	
9	40	914.54	1.0	1.11	4.57	3	69	267	263	43	80	70	
8	42.5	916.03	.97	1.07	6.08	3	69				80	70	
7	45	917.59	1.0	1.11	7.62	3	69				81	71	
6	47.5	919.16	1.0	1.11	9.15	3	69	263	266	44	81	71	
5	50	920.73	.99	1.10	0.68	3	70				81	72	
4	52.5	922.16	.92	1.02	2.15	3	70				81	72	
3	55	923.66	.83	.92	3.55	3	69	266	263	43	81	72	
2	57.5	924.79	.73	.81	4.87	3	68				81	72	
1	60	926.25	.80	.89	6.25	3	68				81	72	
	(0921)												
	0-60	V _m - 35.25		ΔH - .02							AVG. - 72.6		

INTERPOLL LABORATORIES, INC.

(612) 786-6020

Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job Cypress NorthshoreDate 11/13/95 Test 1 Run 2Source Dry Cobble StackNo. of traverse points 12Method 5 Filter holder: glassFilter type: glass fiber

Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 IN.HG (vac) ☒Post test: 0 cfm at 8 IN. HG (vac) ☒

Particulate Catch Data:

No. of filters used:

Recovery solvent(s)

1☒ acetone☐ other(s)

No. of probe wash bottles:

1

Sample recovered by:

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2	197	200	-3
Impinger No. 3			
Condenser			
Desiccant	1498	1484	14
Total			11

Integrated Gas Sampling Data: Ambient airBag Pump No. Box No. Bag No. Bag Material: 5-layer Aluminized TedlarSize: 44 LPretest leak check: cc/min at IN.HGTime start: (HRS) Time end: (HRS)Sampling rate: cc/min Operator: S/N of O₂ Analyzer used to monitor train outlet:

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EPA Method 5 Field Data Sheet

Job C-1005 Northshore Operators J.S. Duff, T.F. Nozzle No. 3-3 Pitot No. U33-5
 Source City Center Stack Meter Box No. 3 AH@ 1.73 in. WC Nozzle Dia. .183 in. 84
 Date 11/3/95 Test 9 Run 2 Gasmer Coeff. 1.000 Bar. Press. 29.03 in. Hg 7 H₂O %

Traverse Point No.	Sampling Time (min)	Sample Vol. (cf)	Velocity Head (in. WC)	Orifice Meter (in. WC)	Des. Vol. (cf)	VAC. (in. Hg)	Temperatures (°F)						Oxygen (% v/v)	
							Stack	Probe	Oven	Imp.	Gas/In	Gas/Out		
	1000	929.92												
12	2.5	931.50	1.03	1.14	1.46	5	68	227	236	46	69	68	Ambient	
11	5	933.10	.97	1.08	2.96	5	67				72	69	AIR	
10	7.5	934.51	.97	1.09	4.47	5	67				74	69		
9	10	936.07	1.03	1.15	6.03	5	68	239	246	47	75	69		
8	12.5	937.57	1.05	1.18	7.61	5	69				76	70		
7	15	939.08	1.05	1.18	9.19	5	68				77	70		
6	17.5	940.55	.93	1.05	0.68	5	68	241	256	47	78	70		
5	20	942.04	.87	.96	2.13	5	68				79	71		
4	22.5	943.57	.87	.98	3.56	5	68				79	71		
3	25	944.98	.80	.90	4.94	5	67	250	257	48	80	71		
2	27.5	946.27	.80	.90	6.26	5	67				80	71		
1	30	947.69	.78	.88	7.63	5	67				80	71		
A 12	32.5	949.16	.92	1.04	9.12	5	67	759	261	49	76	71		
11	35	950.63	.94	1.06	10.61	5	67				81	72		
10	37.5	952.23	.94	1.07	2.12	5	67				81	72		
9	40	953.68	.95	1.08	3.63	5	67	263	261	50	81	72		
8	42.5	955.31	.95	1.08	5.15	5	67				81	72		
7	45	956.69	.94	1.07	6.65	5	67				82	73		
6	47.5	958.31	1.05	1.19	8.25	5	67	267	263	51	82	73		
5	50	959.86	1.10	1.13	9.80	5	68				82	73		
4	52.5	961.43	1.05	1.19	1.39	5	68				82	73		
3	55	962.86	.95	1.08	2.91	5	68	261	263	51	82	73		
2	57.5	964.32	.95	1.08	4.42	5	68				83	73		
1	60	965.85	.83	.94	5.84		67				83	73		
	1.135													
	0.60	35.93		ΔH -1.04							Avg. =	75.1		
		V _m -												

INTERPOLL LABORATORIES, INC.

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Interpoll Laboratories EPA Method 5/17 Sample Log Sheet

Job CYPRES Northshore Date 1/13/95 Test 9 Run 3
 Source Dry Coker Stack No. of traverse points 12
 Method 5 Filter holder: glass Filter type: glass fiber

Sample Train Leak Check:

Pretest: ≤ 0.02 cfm at 15 IN.HG (vac) ☒Post test: 0 cfm at 8 IN. HG (vac) ☒

Particulate Catch Data:

No. of filters used:

Recovery solvent(s)

1

☒ acetone _____☐ other(s) _____

No. of probe wash bottles:

1

Sample recovered by:

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2			
Impinger No. 3	495	500	-5
Condenser			
Desiccant	1502	1495	7
Total	████████████████████		2

Integrated Gas Sampling Data:

Ambient air

Bag Pump No. _____
 Bag Material: 5-layer Aluminized Tedlar
 Pretest leak check: _____
 Time start: _____
 Sampling rate: _____

Box No. _____ Bag No. _____
 Size: 44 L
 cc/min at _____ IN.HG
 (HRS) Time end: _____ (HRS)
 cc/min Operator: _____

S/N of O₂ Analyzer used to monitor train outlet: _____

052394-C:\STACK\WP\FORMS\S-0046RR

EPA Method 5 Field Data Sheet

Job CYPRUS Northshore Operators 3-3 Pilot No. 1/23-5
 Source Duff Coke Stack Meter Box No. 3 ΔH₀ 1.73 in. WC Nozzle Dia. .182 in. C_p 1.84
 Date 1/13/95 Test 7 Run 3 Gasmeter Coeff. 1.000 Bar. Press. 29.02 in. Hg H₂O 1 %

Traverse Point No.	Sampling Time (min)	Sample Vol. (cf)	Velocity Head (in. WC)	Orifice Meter (in. WC)	Des. Vol. (cf)	VAC. (in. Hg)	Temperatures (°F)					Oxygen		
							Stack	Probe	Oven	Imp.	Gas/In	Gas/Out	(% v/v)	
		966.15												
A12	1124	967.63	.89	1.00	7.61	5	68	231	236	46	71	70		Ambient
11	2.5	969.10	.89	1.0	9.05	5	68				70	73		Air
10	5	970.51	.89	1.0	0.50	5	67				75	71		
9	7.5	971.96	.93	1.05	1.99	5	68	246	253	45	77	71		
8	10	973.53	.99	1.11	3.53	5	68				78	71		
7	12.5	975.06	.94	1.06	5.03	5	68				79	72		
6	15	976.45	.96	1.09	6.54	5	67	252	259	46	79	72		
5	17.5	978.04	1.05	1.19	8.13	5	67				81	72		
4	20	979.70	1.05	1.19	9.72	5	67				81	72		
3	22.5	981.25	.93	1.05	1.22	5	67	258	263	47	81	72		
2	25	982.72	.88	1.00	2.67	5	67				82	73		
1	27.5	984.17	.83	.95	4.09	5	69				82	73		
B12	30	985.66	.98	1.11	5.63	5	68	263	262	49	80	73		
11	32.5	987.16	.92	1.04	7.12	5	68				82	73		
10	35	988.71	.94	1.07	8.62	5	68				83	74		
9	37.5	990.24	1.0	1.14	9.18	5	67	266	263	50	83	74		
8	40	991.76	.98	1.11	1.72	5	68				83	74		
7	42.5	993.30	1.1	1.25	3.36	5	68				83	74		
6	45	994.96	1.1	1.25	4.99	5	67	266	263	51	83	74		
5	47.5	996.61	1.03	1.17	6.57	5	68				83	74		
4	50	998.06	.89	1.01	8.04	5	67				83	75		
3	52.5	999.42	.87	.99	9.50	5	67	269	264	51	83	75		
2	55	1000.88	.79	.9	0.89	5	67				83	75		
1	57.6	1002.16	.71	.81	2.20	5	67				83	75		
	60													
	1226													
	0-60	V _m -		ΔT - 11.10							Avg. -	76.6		

Visible Emissions Form

Test #1

SOURCE NAME		OBSERVATION DATE		START TIME		STOP TIME					
Dry Storage Bin		1-10-95		1-10-95							
ADDRESS		SEC	0	15	30	45	MIN	0	15	30	45
Cypress Northshore Mining		1					31				
		2					32				
CITY	STATE	3					33				
Silver Bay	MM	4					34				
PHONE	SOURCE ID NUMBER	5					35				
PROCESS EQUIPMENT	OPERATING MODE	6					36				
CONTROL EQUIPMENT	OPERATING MODE	7					37				
DESCRIBE EMISSION POINT		8					38				
START	STOP	9					39				
HEIGHT ABOVE GROUND LEVEL	HEIGHT RELATIVE TO OBSERVER	10					40				
START	STOP	11					41				
DISTANCE FROM OBSERVER	DIRECTION FROM OBSERVER	12					42				
START	STOP	13					43				
DESCRIBE EMISSIONS		14					44				
START	STOP	15					45				
EMISSION COLOR	PLUME TYPE. CONTINUOUS ☐	16					46				
START	FUGITIVE ☐ INTERMITTENT ☐	17					47				
WATER DROPLETS PRESENT:	IF WATER DROPLET PLUME:	18					48				
NO ☐ YES ☐	ATTACHED ☐ DETACHED ☐	19					49				
POINT IN THE PLUME AT WHICH OPACITY WAS DETERMINED		20					50				
START	STOP	21					51				
DESCRIBE BACKGROUND		22					52				
START	STOP	23					53				
BACKGROUND COLOR	SKY CONDITIONS	24					54				
START	STOP	25					55				
WIND SPEED	WIND DIRECTION	26					56				
START	STOP	27					57				
AMBIENT TEMP.	WET BULB TEMP.	28					58				
START	RH. percent	29					59				
		30					60				
Source Layout Sketch		AVERAGE OPACITY FOR HIGHEST PERIOD									
Draw North Arrow		NUMBER OF READINGS ABOVE % WERE									
		RANGE OF OPACITY READINGS									
		MINIMUM									
		MAXIMUM									
		OBSERVER'S NAME (PRINT)									
		OBSERVER'S SIGNATURE									
		DATE									
		ORGANIZATION									
		CERTIFIED BY									
		DATE									
		VERIFIED BY									
		DATE									
COMMENTS		I HAVE RECEIVED A COPY OF THESE OPACITY OBSERVATIONS									
could not be read - snow		SIGNATURE									
		TITLE									
		DATE									

Visible Emissions Form

Test # 7

SOURCE NAME No 2 Boiler Stack		OBSERVATION DATE 1/12/95		START TIME		STOP TIME	
ADDRESS Northshore Mining		SEC MIN	0	15	30	45	SEC MIN
		1					31
		2					32
CITY Silver Bay	STATE MN	3					33
PHONE	SOURCE ID NUMBER	4					34
PROCESS EQUIPMENT		OPERATING MODE		5			35
CONTROL EQUIPMENT		OPERATING MODE		6			36
		7					37
DESCRIBE EMISSION POINT		8					38
START STOP		9					39
HEIGHT ABOVE GROUND LEVEL		HEIGHT RELATIVE TO OBSERVER		10			40
START STOP		START STOP		11			41
DISTANCE FROM OBSERVER		DIRECTION FROM OBSERVER		12			42
START STOP		START STOP		13			43
DESCRIBE EMISSIONS		14					44
START STOP		15					45
EMISSION COLOR		PLUME TYPE: CONTINUOUS ☐		16			46
START STOP		FUGITIVE ☐ INTERMITTENT ☐		17			47
WATER DROPLETS PRESENT:		IF WATER DROPLET PLUME:		18			48
NO ☐ YES ☐		ATTACHED ☐ DETACHED ☐		19			49
POINT IN THE PLUME AT WHICH OPACITY WAS DETERMINED		20					50
START STOP		21					51
DESCRIBE BACKGROUND		22					52
START STOP		23					53
BACKGROUND COLOR		SKY CONDITIONS		24			54
START STOP		START STOP		25			55
WIND SPEED		WIND DIRECTION		26			56
START STOP		START STOP		27			57
AMBIENT TEMP.		WET BULB TEMP.		28			58
START STOP		RH, percent		29			59
		30					60
Source Layout Sketch Draw North Arrow Sun → Wind → Plume and Stack X Emission Point Observers Position 140° Sun Location Line				AVERAGE OPACITY FOR HIGHEST PERIOD RANGE OF OPACITY READINGS MINIMUM MAXIMUM NUMBER OF READINGS ABOVE % WERE			
COMMENTS could not be done drizzle & fog				OBSERVER'S NAME (PRINT) Jeff Scriber			
				OBSERVER'S SIGNATURE <i>Jeff Scriber</i>		DATE 1/12/95	
				ORGANIZATION Interpoll			
I HAVE RECEIVED A COPY OF THESE OPACITY OBSERVATIONS				CERTIFIED BY ETA		DATE 10/9/94	
SIGNATURE		DATE		VERIFIED BY		DATE	
TITLE		DATE		VERIFIED BY		DATE	

Visible Emissions Form

Test # 9

SOURCE NAME			OBSERVATION DATE			START TIME			STOP TIME			
Dr. Coker Stick			1/13/95			1/13/95						
ADDRESS			SEC	0	15	30	45	MIN	0	15	30	45
Cyprian Northshore Mining			1					31				
CITY			2					32				
Silver Bay			3					33				
STATE			4					34				
MN			5					35				
ZIP			6					36				
PHONE			7					37				
SOURCE ID NUMBER			8					38				
PROCESS EQUIPMENT			9					39				
OPERATING MODE			10					40				
CONTROL EQUIPMENT			11					41				
OPERATING MODE			12					42				
DESCRIBE EMISSION POINT			13					43				
START			14					44				
STOP			15					45				
HEIGHT ABOVE GROUND LEVEL			16					46				
HEIGHT RELATIVE TO OBSERVER			17					47				
START			18					48				
STOP			19					49				
DISTANCE FROM OBSERVER			20					50				
DIRECTION FROM OBSERVER			21					51				
START			22					52				
STOP			23					53				
DESCRIBE EMISSIONS			24					54				
START			25					55				
STOP			26					56				
EMISSION COLOR			27					57				
PLUME TYPE: CONTINUOUS ☐			28					58				
FUGITIVE ☐ INTERMITTENT ☐			29					59				
WATER DROPLETS PRESENT: NO ☐ YES ☐			30					60				
IF WATER DROPLET PLUME: ATTACHED ☐ DETACHED ☐			AVERAGE OPACITY FOR HIGHEST PERIOD			NUMBER OF READINGS ABOVE % WERE						
POINT IN THE PLUME AT WHICH OPACITY WAS DETERMINED			RANGE OF OPACITY READINGS			MINIMUM			MAXIMUM			
START			OBSERVER'S NAME (PRINT)			Jett Script						
STOP			OBSERVER'S SIGNATURE			UPH Starts			DATE 1/13/95			
BACKGROUND COLOR			ORGANIZATION			Interpoll						
SKY CONDITIONS			CERTIFIED BY			ETA			DATE 10/9/94			
WIND SPEED			VERIFIED BY						DATE			
WIND DIRECTION												
START												
STOP												
AMBIENT TEMP.												
WET BULB TEMP												
RH. percent												
START												
STOP												
Source Layout Sketch Draw North Arrow												
COMMENTS could not be done heavy snow												
I HAVE RECEIVED A COPY OF THESE OPACITY OBSERVATIONS												
SIGNATURE												
TITLE												
DATE												

VISIBLE EMISSIONS EVALUATOR

This is to certify that

Q-66 Chexipster

met the specifications of Federal Reference Method 9 and qualified as a visible emissions evaluator. Maximum deviation on white and black smoke did not exceed 7.5% opacity and no single error exceeding 15% opacity was incurred during the certification test conducted by Eastern Technical Associates of Raleigh, North Carolina. This certificate is valid for six months from date of issue.

Thomas Lane
President

245683
Certificate Number

William S. Lane
Vice President

Memmiapolis
Location

David B. Savage, Jr.
Program Manager

October 5 1994
Date of Issue

APPENDIX D

INTERPOLL LABORATORIES ANALYTICAL DATA

EPA Method 3 Data Reporting Sheet
Orsat Analysis

Job Cyprus Northshore Mining
 Team Leader DVH
 Date Submitted 1-16-95
 Test No. 2
 Date of Analysis 1-16-95

Source No. 1105 Pelletizer
 Test Site Stack
 Date of Test 1-10-95
 No. of Runs Completed 3
 Technician B. Drake

Test/ Run	Sample Log Number and Type	No. of An.	Buret Readings (ml)			Conc. CO ₂ %v/v Dry	Conc. O ₂ %v/v Dry	F _o
			Zero Pt.	After CO ₂	After O ₂			
2/1	4664-09 ☒ B ☐ F	1	0.00	1.80	19.00	1.80	17.20	
		2	0.00	1.80	19.00	1.80	17.20	
		Avg				1.80	17.20	
2/2	-10 ☒ B ☐ F	1	0.00	1.80	19.10	1.80	17.30	
		2	0.00	1.80	19.10	1.80	17.30	
		Avg				1.80	17.30	
2/3	-11 ☒ B ☐ F	1	0.00	1.80	19.00	1.80	17.20	
		2	0.00	1.80	19.00	1.80	17.20	
		Avg				1.80	17.20	
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						
	☐ B ☐ F	1						
		2						
		Avg						

- ☒ Ambient Air QA Check
☒ Orsat Analyzer System Leak Check
☐ F_o Within EPA M-3 Guidelines
 for fuel type.

Where $F_o = \frac{20.9 - O_2}{CO_2}$

EPA Method 3 Guidelines
Fuel Type F_o Range

Coal:	
Anthracite/Lignite	1.016-1.130
Bituminous	1.083-1.230
Oil:	
Distillate	1.260-1.413
Residual	1.210-1.370
Gas:	
Natural	1.600-1.836
Propane	1.434-1.586
Butane	1.405-1.553
Wood/Wood Bark	1.000-1.130

F=Flask (250 cc all glass)
 B=Tedlar Bag (5-layer)

D-1

LSC-04-BR

EPA Method 3 Data Reporting Sheet
Orsat Analysis

Job Cyprus Northshore Mining
 Team Leader DOH
 Date Submitted 1-16-95
 Test No. 4
 Date of Analysis 1-16-95

Source No. 1205 Waste Gas
 Test Site Stack
 Date of Test 1-11-95
 No. of Runs Completed 3
 Technician MDP

Test/ Run	Sample Log Number and Type	No. of An.	Buret Readings (ml)			Conc. CO ₂ %v/v Dry	Conc. O ₂ %v/v Dry	F ₀
			Zero Pt.	After CO ₂	After O ₂			
4/1	4664-23 □ B □ F	1	0.00	2.10	18.90	2.10	16.80	
		2	0.00	2.10	18.90	2.10	16.80	
		Avg				2.10	16.80	
4/2	-24 □ B □ F	1	0.00	2.00	18.80	2.00	16.80	
		2	0.00	2.00	18.80	2.00	16.80	
		Avg				2.00	16.80	
4/3	-25 □ B □ F	1	0.00	2.00	19.00	2.00	17.00	
		2	0.00	2.00	19.00	2.00	17.00	
		Avg				2.00	17.00	
	□ B □ F	1						
		2						
		Avg						
	□ B □ F	1						
		2						
		Avg						
	□ B □ F	1						
		2						
		Avg						
	□ B □ F	1						
		2						
		Avg						
	□ B □ F	1						
		2						
		Avg						
	□ B □ F	1						
		2						
		Avg						

- ☒ Ambient Air QA Check
☒ Orsat Analyzer System Leak Check
☐ F₀ Within EPA M-3 Guidelines
 for fuel type.

Where $F_0 = \frac{20.9 - O_2}{CO_2}$

EPA Method 3 Guidelines	
Fuel Type	F ₀ Range
Coal:	
Anthracite/Lignite	1.016-1.130
Bituminous	1.083-1.230
Oil:	
Distillate	1.260-1.413
Residual	1.210-1.370
Gas:	
Natural	1.600-1.936
Propane	1.434-1.596
Butane	1.405-1.553
Wood/Wood Bark	1.000-1.130

F=Flask (250 cc all glass)
 B=Tedlar Bag (5-layer)

D-3

LSC-04-BR

EPA Method 3 Data Reporting Sheet
Orsat Analysis

Job Cyprus North Shore Mining
 Team Leader GH
 Date Submitted 1-16-95
 Test No. 6
 Date of Analysis 1-16-95

Source No. 12 Rotocone - North
 Test Site Stack
 Date of Test 1-12-95
 No. of Runs Completed 3
 Technician A. White

Test/ Run	Sample Log Number and Type	No. of An.	Buret Readings (ml)			Conc. CO ₂ %v/v Dry	Conc. O ₂ %v/v Dry	F _o
			Zero Pt.	After CO ₂	After O ₂			
6/1	4664-50 □ B □ F	1	0.00	0.00	20.90	0.00	20.90	
		2	0.00	0.00	20.90	0.00	20.90	
		Avg				0.00	20.90	
6/2	-51 □ B □ F	1	0.00	0.00	20.90	0.00	20.90	
		2	0.00	0.00	20.90	0.00	20.90	
		Avg				0.00	20.90	
6/3	-52 □ B □ F	1	0.00	0.00	20.90	0.00	20.90	
		2	0.00	0.00	20.90	0.00	20.90	
		Avg				0.00	20.90	
	□ B □ F	1						
		2						
		Avg						
	□ B □ F	1						
		2						
		Avg						
	□ B □ F	1						
		2						
		Avg						
	□ B □ F	1						
		2						
		Avg						
	□ B □ F	1						
		2						
		Avg						
	□ B □ F	1						
		2						
		Avg						

- ☒ Ambient Air QA Check
☒ Orsat Analyzer System Leak Check
☐ F_o Within EPA M-3 Guidelines
 for fuel type.

Where $F_o = \frac{20.9 - O_2}{CO_2}$

F=Flask (250 cc all glass)
 B=Tedlar Bag (5-layer)

D-5

EPA Method 3 Guidelines

Fuel Type	F _o Range
Coal:	
Anthracite/Lignite	1.016-1.130
Bituminous	1.083-1.230
Oil:	
Distillate	1.260-1.413
Residual	1.210-1.370
Gas:	
Natural	1.600-1.936
Propane	1.434-1.586
Butane	1.405-1.553
Wood/Wood Bark	1.000-1.130

LSC-04-BR

INTERPOLL LABORATORIES, INC.

(612) 786-6020

Impinger Catch Data Reporting Sheet

Protocol: ☒ Minnesota ☐ Wisconsin ☐ Iowa☐ EPA Method 202 ☐ OtherJob: Cypress North ShoreSource/Site: Bin SturgeDate Submitted: 1-16-95Test No.: 1Date of Analysis: 1-17-95Technician: J. Lopez

		Solvent Phase		Aqueous Phase	
Test: 1	Run: 0	Dish No: 1		Dish No:	
Log No: 4664 - 01 I		Dish + Sample Wt: 56.9700 g		Dish + Sample Wt:	
Color & Appearance:		Dish Tare Wt: 56.9696 g		Dish Tare Wt:	
		Fraction Wt: .0004 g		Fraction Wt:	
Comments: Field Blank		Smpl Vol: ml, Alqt: ml, Factor: 1.000		Smpl Vol: ml, Alqt: ml, Factor:	
		Sample Wt: .0004 g		Sample Wt:	
Test: 1	Run: 1	Dish No: 3		Dish No:	
Log No: -02 I		Dish + Sample Wt: 43.8915 g		Dish + Sample Wt:	
Color & Appearance:		Dish Tare Wt: 43.8910 g		Dish Tare Wt:	
		Fraction Wt: .0005 g		Fraction Wt:	
Comments:		Smpl Vol: ml, Alqt: ml, Factor: 1.000		Smpl Vol: ml, Alqt: ml, Factor:	
		Sample Wt: .0005 g		Sample Wt:	
Test: 1	Run: 2	Dish No: 25		Dish No:	
Log No: -03 I		Dish + Sample Wt: 44.3447 g		Dish + Sample Wt:	
Color & Appearance:		Dish Tare Wt: 44.3435 g		Dish Tare Wt:	
		Fraction Wt: .0012 g		Fraction Wt:	
Comments:		Smpl Vol: ml, Alqt: ml, Factor: 1.000		Smpl Vol: ml, Alqt: ml, Factor:	
		Sample Wt: .0012 g		Sample Wt:	
Test: 1	Run: 3	Dish No: 27		Dish No:	
Log No: -04 I		Dish + Sample Wt: 52.4460 g		Dish + Sample Wt:	
Color & Appearance:		Dish Tare Wt: 52.4444 g		Dish Tare Wt:	
		Fraction Wt: .0016 g		Fraction Wt:	
Comments:		Smpl Vol: ml, Alqt: ml, Factor: 1.000		Smpl Vol: ml, Alqt: ml, Factor:	
		Sample Wt: .0016 g		Sample Wt:	

Note: Factor = Sample Volume/Aliquot Volume

Blank Solvent Wt. .0001 g

	RUN 0 Field Blank	RUN 1	RUN 2	RUN 3
Results of Solvent Phase	.0004	.0001	.0008	.0012
Results of Aqueous Phase	D-7			



EPA Method 5 Data Reporting Sheet Probe/Cyclone Wash

Job North Shore Mining Source Ben Storage
 Team Leader ET Test Site Stack
 Date Submitted 1/16/95 Date of Test 1/10/95
 Test No. 1 No. of Runs 3
 Date of Analysis 1/16/95 Technician KT
 Transport Leakage ☐ None ☒ ml Solvent Acetone

Test:	1 Run: 0	Dish No:	731 -
Field Blank:		Dish Tare Wt:	45.6745 g
Log No:	4664-01P	Dish + Sample Wt:	45.6747 g
Volume of Solvent	120 ml	Sample Wt:	0.0002 g
*Solvent Residue	1.67 ug/ml		
Test:	1 Run: 1	Dish No:	738 -
Vol. of Solvent	130 ml	Dish Tare Wt:	44.9282 g
Log Number	-02P	Dish + Sample Wt:	44.9370 g
Comments		Sample Wt:	0.0088 g
Test:	1 Run: 2	Dish No:	739 -
Vol. of Solvent	140 ml	Dish Tare Wt:	45.3591 g
Log Number	-03P	Dish + Sample Wt:	45.3681 g
Comments		Sample Wt:	0.0090 g
Test:	1 Run: 3	Dish No:	740 -
Vol. of Solvent	130 ml	Dish Tare Wt:	44.9522 g
Log Number	-04P	Dish + Sample Wt:	44.9610 g
Comments		Sample Wt:	0.0088 g
Test:	Run:	Dish No:	
Log No:		Dish Tare Wt:	g
Comments:		Dish + Sample Wt:	g
		Sample Wt:	g
Test:	Run:	Dish No:	
Vol of Solvent	ml	Dish Tare Wt:	g
Log Number		Dish + Sample Wt:	g
Comments		Sample Wt:	g

*Solvent Residue 1.67 ug/ml = [(Sample Wt. 0.0088 g) (10⁶)] / Vol. of Sol. 120 ml

EPA-M5 Acetone Residue Blank Spec. ≤ 7.8 ug/ml

Results:

Blank Solvent Wt. 0.0002

Field Blank	Run 1	Run 2	Run 3	Run 4	Run 5
	0.0086	0.0088	0.0086	0.0086	

Job	<u>North Shore Mining</u>	Source	<u>Bun Storage</u>
Team Leader	<u>ET</u>	Test Site	<u>Stack</u>
Date Submitted	<u>1/16/95</u>	Date of Test	<u>1/10/95</u>
Test No.	<u>1</u>	No. of Runs	<u>3</u>
Date of Analysis	<u>1/16/95</u>	Technician	<u>KT</u>

Test:	1 Run: 0	Filter No:	6761
Field Blank:		Filter Type:	4"GF
Log No:	4664-01F	Filter Tare Wt:	0.9490 g
Comments:		Filter + Sample Wt:	0.9495 g
		Sample Wt:	0.0005 g
Test:	1 Run: 1	Filter No:	6756
Log No:	-02F	Filter Type:	4"GF
Comments:		Filter Tare Wt:	0.9402 g
		Filter + Sample Wt:	0.9433 g
		Sample Wt:	0.0031 g
Test:	1 Run: 2	Filter No:	6755
Log No:	-03F	Filter Type:	4"GF
Comments:		Filter Tare Wt:	0.9237 g
		Filter + Sample Wt:	0.9281 g
		Sample Wt:	0.0044 g
Test:	1 Run: 3	Filter No:	6759
Log No:	-04F	Filter Type:	4"GF
Comments:		Filter Tare Wt:	0.9296 g
		Filter + Sample Wt:	0.9358 g
		Sample Wt:	0.0062 g
Test:	Run:	Filter No:	
Log No:		Filter Type:	
Comments:		Filter Tare Wt:	g
		Filter + Sample Wt:	g
		Sample Wt:	g
Test:	Run:	Filter No:	
Log No:		Filter Type:	
Comments:		Filter Tare Wt:	g
		Filter + Sample Wt:	g
		Sample Wt:	g

Results:

Field Blank	Run 1	Run 2	Run 3	Run 4	Run 5
	0.0031	0.0044	0.0062		

Field Blk.	Run 1	Run 2	Run 3	Run 4	Run 5
	0.0118	0.0140	0.0160		

INTERPOLL LABORATORIES, INC.

(612) 786-6020

Impinger Catch Data Reporting Sheet

Protocol: ☒ Minnesota ☐ Wisconsin ☐ Iowa☐ EPA Method 202 ☐ OtherJob: North ShoreSource/Site: No 1105 Pollution / 5 truckDate Submitted: 1-16-95Test No.: 2Date of Analysis: 1-18-95Technician: J. Lorenz

		Solvent Phase		Aqueous Phase	
Test: <u>2</u>	Run: <u>0</u>	Dish No: <u>60</u>		Dish No:	
Log No: <u>41664-05 I</u>		Dish + Sample Wt: <u>43.5640</u> g		Dish + Sample Wt:	
Color & Appearance:		Dish Tare Wt: <u>43.5635</u> g		Dish Tare Wt:	
		Fraction Wt: <u>.0005</u> g		Fraction Wt:	
Comments: <u>Field Blank</u>		Smpl Vol: ml, Alqt: ml, Factor: <u>1.000</u>		Smpl Vol: ml, Alqt: ml, Factor:	
		Sample Wt: <u>.0005</u> g		Sample Wt:	
Test: <u>2</u>	Run: <u>1</u>	Dish No: <u>68</u>		Dish No:	
Log No: <u>-06 I</u>		Dish + Sample Wt: <u>43.1590</u> g		Dish + Sample Wt:	
Color & Appearance:		Dish Tare Wt: <u>43.1549</u> g		Dish Tare Wt:	
		Fraction Wt: <u>.0041</u> g		Fraction Wt:	
Comments:		Smpl Vol: ml, Alqt: ml, Factor: <u>1.000</u>		Smpl Vol: ml, Alqt: ml, Factor:	
		Sample Wt: <u>.0041</u> g		Sample Wt:	
Test: <u>2</u>	Run: <u>2</u>	Dish No: <u>340</u>		Dish No:	
Log No: <u>-07 I</u>		Dish + Sample Wt: <u>47.9175</u> g		Dish + Sample Wt:	
Color & Appearance:		Dish Tare Wt: <u>47.9145</u> g		Dish Tare Wt:	
		Fraction Wt: <u>.0030</u> g		Fraction Wt:	
Comments:		Smpl Vol: ml, Alqt: ml, Factor: <u>1.000</u>		Smpl Vol: ml, Alqt: ml, Factor:	
		Sample Wt: <u>.0030</u> g		Sample Wt:	
Test: <u>2</u>	Run: <u>3</u>	Dish No: <u>404</u>		Dish No:	
Log No: <u>-08 I</u>		Dish + Sample Wt: <u>47.6438</u> g		Dish + Sample Wt:	
Color & Appearance:		Dish Tare Wt: <u>47.6395</u> g		Dish Tare Wt:	
		Fraction Wt: <u>.0043</u> g		Fraction Wt:	
Comments:		Smpl Vol: ml, Alqt: ml, Factor: <u>1.000</u>		Smpl Vol: ml, Alqt: ml, Factor:	
		Sample Wt: <u>.0043</u> g		Sample Wt:	

Note: Factor = Sample Volume/Aliquot Volume

Blank Solvent Wt: .0001 g

	RUN 0	RUN 1	RUN 2	RUN 3
Results of Solvent Phase	.0005	.0030	.0025	.0038
Results of Aqueous Phase	D-10			



EPA Method 5 Data Reporting Sheet Probe/Cyclone Wash

Job: <u>North Shore - Cyprus</u>	Source: <u>No 1105 Pellitizer</u>
Team Leader: <u>DVH</u>	Test Site: <u>Stack</u>
Date Submitted: <u>1/16/95</u>	Date of Test: <u>1/10/95</u>
Test No.: <u>2</u>	No. of Runs: <u>3</u>
Date of Analysis: <u>1/16/95</u>	Technician: <u>KT</u>
Transport Leakage: ☐ <u>None</u> ☒ <u>ml</u>	Solvent: <u>Acetone</u>

Test: <u>2</u> Run: <u>0</u>	Dish No: <u>820</u>
Field Blank:	Dish Tare Wt: <u>44.1965</u> g
Log No: <u>4664-OSP</u>	Dish + Sample Wt: <u>44.1970</u> g
Volume of Solvent <u>130</u> ml	Sample Wt: <u>0.0005</u> g
*Solvent Residue <u>3.85</u> ug/ml	
Test: <u>2</u> Run: <u>1</u>	Dish No: <u>791</u>
Vol. of Solvent <u>200</u> ml	Dish Tare Wt: <u>44.0824</u> g
Log Number <u>-06P</u>	Dish + Sample Wt: <u>44.1029</u> g
Comments:	Sample Wt: <u>0.0205</u> g
Test: <u>2</u> Run: <u>2</u>	Dish No: <u>792</u>
Vol. of Solvent <u>240</u> ml	Dish Tare Wt: <u>47.2562</u> g
Log Number <u>-07P</u>	Dish + Sample Wt: <u>47.2812</u> g
Comments:	Sample Wt: <u>0.0250</u> g
Test: <u>2</u> Run: <u>3</u>	Dish No: <u>793</u>
Vol. of Solvent <u>160</u> ml	Dish Tare Wt: <u>45.9574</u> g
Log Number <u>-08P</u>	Dish + Sample Wt: <u>45.9805</u> g
Comments:	Sample Wt: <u>0.0231</u> g
Test: Run:	Dish No:
Log No:	Dish Tare Wt:
Comments:	Dish + Sample Wt:
	Sample Wt:
Test: Run:	Dish No:
Vol of Solvent ml	Dish Tare Wt:
Log Number	Dish + Sample Wt:
Comments	Sample Wt:

*Solvent Residue 3.85 ug/ml = [(Sample Wt. 0.0005 g) (10⁶)]/Vol. of Sol. 130 ml

EPA-M5 Acetone Residue Blank Spec. ≤ 7.8 ug/ml

Results:

Blank Solvent Wt. 0.0005

Field Blank	Run 1	Run 2	Run 3	Run 4	Run 5
	<u>0.0197</u>	<u>0.0240</u>	<u>0.0225</u>	<u>0-11</u>	

EPA Method 5 Data Reporting Sheet Filter

Cypress North Shore

DVH

1/16/95

2

1/16/95

Source

Test Site

Date of Test

No. of Runs

Technician

No. 1105 Permeage

Stack

1/10/95

3

KT

2 Run: 0

Filter No:

Filter Type:

Filter Tare Wt:

Filter + Sample Wt:

Sample Wt:

Filter No:

Filter Type:

Filter Tare Wt:

Filter + Sample Wt:

Sample Wt:

2 Run: 2

Filter No:

Filter Type:

Filter Tare Wt:

Filter + Sample Wt:

Sample Wt:

2 Run: 3

Filter No:

Filter Type:

Filter Tare Wt:

Filter + Sample Wt:

Sample Wt:

Run:

Filter No:

Filter Type:

Filter Tare Wt:

Filter + Sample Wt:

Sample Wt:

Run:

Filter No:

Filter Type:

Filter Tare Wt:

Filter + Sample Wt:

Sample Wt:

Comments:

Results:

Field Blank

Run 1

0.0110

Run 2

0.0101

Run 3

0.0115

Run 4

Run 5

Field Blk.

Run 1

0.0343

Run 2

0.0366

Run 3

0.0378

Run 4

Run 5

EPA Method 5 Data Reporting Sheet Probe/Cyclone Wash

Job: <u>Cyprus North Shore</u>	Source: <u>1104 Pelletizer</u>
Team Leader: <u>GH</u>	Test Site: <u>Stack</u>
Date Submitted: <u>1/16/95</u>	Date of Test: <u>1/16/95</u>
Test No.: <u>3</u>	No. of Runs: <u>3</u>
Date of Analysis: <u>1/16/95</u>	Technician: <u>KT</u>
Transport Leakage: ☐ <u>None</u> ml	Solvent: <u>Acetone</u>

Test: <u>3</u> Run: <u>0</u>	Dish No: <u>754</u>
Field Blank:	Dish Tare Wt: <u>45.2821</u> g
Log No: <u>4664-12P</u>	Dish + Sample Wt: <u>45.2826</u> g
Volume of Solvent: <u>110</u> ml	Sample Wt: <u>0.0005</u> g
*Solvent Residue: <u>4.55</u> ug/ml	
Test: <u>3</u> Run: <u>1</u>	Dish No: <u>765</u>
Vol. of Solvent: <u>80</u> ml	Dish Tare Wt: <u>44.1893</u> g
Log Number: <u>4664-13P</u>	Dish + Sample Wt: <u>44.2135</u> g
Comments:	Sample Wt: <u>0.0242</u> g
Test: <u>3</u> Run: <u>2</u>	Dish No: <u>766</u>
Vol. of Solvent: <u>100</u> ml	Dish Tare Wt: <u>42.2415</u> g
Log Number: <u>-14P</u>	Dish + Sample Wt: <u>42.2595</u> g
Comments:	Sample Wt: <u>0.0180</u> g
Test: <u>3</u> Run: <u>3</u>	Dish No: <u>767</u>
Vol. of Solvent: <u>60</u>	Dish Tare Wt: <u>42.4095</u> g
Log Number: <u>-15P</u>	Dish + Sample Wt: <u>42.4164</u> g
Comments:	Sample Wt: <u>0.0069</u> g
Test: Run:	Dish No:
Log No:	Dish Tare Wt:
Comments:	Dish + Sample Wt:
	Sample Wt:
Test: Run:	Dish No:
Vol of Solvent: ml	Dish Tare Wt:
Log Number:	Dish + Sample Wt:
Comments:	Sample Wt:

*Solvent Residue 4.55 ug/ml = [(Sample Wt. 0.0005 g) (10⁶)]/Vol. of Sol. 110 ml

EPA-M5 Acetone Residue Blank Spec. ≤ 7.8 ug/ml

Results:

Blank Solvent Wt. 0.0005

Field Blank	Run 1	Run 2	Run 3	Run 4	Run 5
	<u>0.0238</u>	<u>0.0175</u>	<u>0.0066</u>	<u>D-14</u>	

EPA Method 5 Data Reporting

Cyprus North Shore
 GH
 1/16/95
 3
 1/16/95

Source
 Test Site
 Date of Test
 No. of Runs
 Technician

1104 PENN
 STACK
 1/10/95
 3
 RT

Task

4664-12F	3 Run: 0	Filter No: 7227	Filter Type: 4"GF.	Filter Tare Wt: 0.9115	Filter + Sample Wt: 0.9116	Sample Wt: 0.0001
-13F	3 Run: 1	Filter No: 7048	Filter Type: 4"GF	Filter Tare Wt: 0.9576	Filter + Sample Wt: 0.9716	Sample Wt: 0.0140
-14F	3 Run: 2	Filter No: 7049	Filter Type: 4"GF	Filter Tare Wt: 0.9675	Filter + Sample Wt: 0.9784	Sample Wt: 0.0109
-15F	3 Run: 3	Filter No: 7110	Filter Type: 4"GF	Filter Tare Wt: 0.9437	Filter + Sample Wt: 0.9557	Sample Wt: 0.0120
	Run:	Filter No:	Filter Type:	Filter Tare Wt:	Filter + Sample Wt:	Sample Wt:
	Run:	Filter No:	Filter Type:	Filter Tare Wt:	Filter + Sample Wt:	Sample Wt:

Results:	Run 1	Run 2	Run 3	Run 4	Run 5
Field Blank	0.0140	0.0109	0.0120		
Field Blk.	0.0391	0.0296	0.0209		

080594-G:STACKIWPFORMSS-491

EPA Method 5 Data Reporting Sheet Probe/Cyclone Wash

Job	<u>Cypus North Shore</u>	Source	<u>No 1205 Waste Gas</u>
Team Leader	<u>DVH</u>	Test Site	<u>Stack</u>
Date Submitted	<u>1/16/95</u>	Date of Test	<u>1/11/95</u>
Test No.	<u>4</u>	No. of Runs	<u>3</u>
Date of Analysis	<u>1/16/95</u>	Technician	<u>KT</u>
Transport Leakage ☐	<u>None</u>	Solvent	<u>Acetone</u>

Test: <u>4</u> Run: <u>0</u>	Dish No: <u>728</u>
Field Blank: <u>130</u>	Dish Tare Wt: <u>42.9797</u> g
Log No: <u>4664-19P</u>	Dish + Sample Wt: <u>42.9798</u> g
Volume of Solvent: <u>100</u> ml	Sample Wt: <u>0.0001</u> g
*Solvent Residue: <u>1.0</u> ug/ml	
Test: <u>4</u> Run: <u>1</u>	Dish No: <u>744</u>
Vol. of Solvent: <u>200</u> ml	Dish Tare Wt: <u>48.6333</u> g
Log Number: <u>-20P</u>	Dish + Sample Wt: <u>48.6515</u> g
Comments:	Sample Wt: <u>0.0182</u> g
Test: <u>4</u> Run: <u>2</u>	Dish No: <u>796</u>
Vol. of Solvent: <u>200</u> ml	Dish Tare Wt: <u>44.7964</u> g
Log Number: <u>-21P</u>	Dish + Sample Wt: <u>44.8114</u> g
Comments:	Sample Wt: <u>0.0150</u> g
Test: <u>4</u> Run: <u>3</u>	Dish No: <u>797</u>
Vol. of Solvent: <u>190</u> ml	Dish Tare Wt: <u>43.0471</u> g
Log Number: <u>-22P</u>	Dish + Sample Wt: <u>43.0619</u> g
Comments:	Sample Wt: <u>0.0148</u> g
Test: Run:	Dish No:
Log No:	Dish Tare Wt: g
Comments:	Dish + Sample Wt: g
	Sample Wt: g
Test: Run:	Dish No:
Vol of Solvent ml	Dish Tare Wt: g
Log Number	Dish + Sample Wt: g
Comments	Sample Wt: g

*Solvent Residue 1.0 ug/ml = [(Sample Wt. 0.0018 g) (10⁶)] / Vol. of Sol. 180 ml

EPA-M5 Acetone Residue Blank Spec. ≤ 7.8 ug/ml

Results:

Blank Solvent Wt. 0.0001

Field Blank	Run 1	Run 2	Run 3	Run 4	Run 5
	<u>0.0180</u>	<u>0.0148</u>	<u>0.0146</u>	<u>0-17</u>	

EPA Method 5 Data Reporting Sheet

Cyprus North Shore

DVH

1/16/95

4

1/16/95

Source

Test Site

Date of Test

No. of Runs

Technician

No 1205 was a

Stack

1/11/95

3

Rt

4 Run: 0

Filter No:

7100

Filter Type:

4"GF

Filter Tare Wt:

0.9479

Filter + Sample Wt:

0.9480

Sample Wt:

0.0001

Filter No:

7065

Filter Type:

4"GF

Filter Tare Wt:

0.9472

Filter + Sample Wt:

0.9549

Sample Wt:

0.0077

4 Run: 2

Filter No:

7064

Filter Type:

4"GF

Filter Tare Wt:

0.9520

Filter + Sample Wt:

0.9609

Sample Wt:

0.0089

4 Run: 3

Filter No:

7066

Filter Type:

4"GF

Filter Tare Wt:

0.9396

Filter + Sample Wt:

0.9476

Sample Wt:

0.0080

Run:

Filter No.

Filter Type:

Filter Tare Wt:

Filter + Sample Wt:

Sample Wt:

Run:

Filter No:

Filter Type:

Filter Tare Wt:

Filter + Sample Wt:

Sample Wt:

Results:

Field Blank

Run 1

0.0077

Run 2

0.0089

Run 3

0.0080

Run 4

Run 5

Field Blk.

Run 1

0.0297

Run 2

0.0281

Run 3

0.0273

Run 4

Run 5

EPA Method 5 Data Reporting Sheet Probe/Cyclone Wash

Job Cypus North Shore Source 1204 Waste Gas
 Team Leader GH Test Site Stack
 Date Submitted 1/16/95 Date of Test 1/11/95
 Test No. 5 No. of Runs 3
 Date of Analysis 1/16/95 Technician KT
 Transport Leakage ☐ None ☒ ml Solvent Acetone

Test: <u>5</u> Run: <u>0</u>	Dish No: <u>4</u>
Field Blank:	Dish Tare Wt: <u>47.3797</u> g
Log No: <u>4664-39P</u>	Dish + Sample Wt: <u>47.3802</u> g
Volume of Solvent <u>130</u> ml	Sample Wt: <u>0.0005</u> g
*Solvent Residue <u>3.85</u> ug/ml	
Test: <u>5</u> Run: <u>1</u>	Dish No: <u>6</u>
Vol. of Solvent <u>100</u> ml	Dish Tare Wt: <u>48.2716</u> g
Log Number <u>-40P</u>	Dish + Sample Wt: <u>48.2838</u> g
Comments	Sample Wt: <u>0.0122</u> g
Test: <u>5</u> Run: <u>2</u>	Dish No: <u>8</u>
Vol. of Solvent <u>80</u> ml	Dish Tare Wt: <u>46.9757</u> g
Log Number <u>-41P</u>	Dish + Sample Wt: <u>46.9820</u> g
Comments	Sample Wt: <u>0.0063</u> g
Test: <u>5</u> Run: <u>3</u>	Dish No: <u>9</u>
Vol. of Solvent <u>110</u> ml	Dish Tare Wt: <u>43.6647</u> g
Log Number <u>-42P</u>	Dish + Sample Wt: <u>43.6748</u> g
Comments	Sample Wt: <u>0.0101</u> g
Test: Run:	Dish No:
Log No:	Dish Tare Wt: g
Comments:	Dish + Sample Wt: g
	Sample Wt: g
Test: Run:	Dish No:
Vol of Solvent ml	Dish Tare Wt: g
Log Number	Dish + Sample Wt: g
Comments	Sample Wt: g

*Solvent Residue 3.85 ug/ml = [(Sample Wt 0.0122 g) (10⁶)] / Vol. of Sol. 130 ml

EPA-M5 Acetone Residue Blank Spec. ≤ 7.8 ug/ml

Results:

Blank Solvent Wt. 0.0005

Field Blank	Run 1	Run 2	Run 3	Run 4	Run 5
	<u>0.0118</u>	<u>0.0060</u>	<u>0.0047</u>	<u>0.20</u>	

EPA Method 5 Data Reporting Sheet

Cyprus North Shore

GH

1/16/95

5

Source

Test Site

Date of Test

No. of Runs

Technician

12044 Wacker

Stack

1/11/95

3

RT

3 runs

5 Run: 0

Filter No:

7225

Filter Type:

4"GF

Filter Tare Wt:

0.9135

Filter + Sample Wt:

0.9135

Sample Wt:

0.0000

5 Run: 1

Filter No:

7111

Filter Type:

4"GF

Filter Tare Wt:

0.9489

Filter + Sample Wt:

0.9602

Sample Wt:

0.0113

5 Run: 2

Filter No:

7112

Filter Type:

4"GF

Filter Tare Wt:

0.9514

Filter + Sample Wt:

0.9635

Sample Wt:

0.0121

5 Run: 3

Filter No:

7113

Filter Type:

4"GF

Filter Tare Wt:

0.9467

Filter + Sample Wt:

0.9586

Sample Wt:

0.0119

Run:

Filter No.

Filter Type:

Filter Tare Wt:

Filter + Sample Wt:

Sample Wt:

Run:

Filter No:

Filter Type:

Filter Tare Wt:

Filter + Sample Wt:

Sample Wt:

Results:

Field Blank

Run 1

0.0113

Run 2

0.0121

Run 3

0.0114

Run 4

Run 5

Field Blk.

Run 1

0.0240

Run 2

0.0184

Run 3

0.0233

Run 4

Run 5

D-21

080594-G:STACKWPMFORMSS-491

INTERPOL LABORATORIES, INC.
(612) 786-6020
Solvent Rinse Data Reporting Sheet

☒ EPA Method 5 Probe Wash ☐ EPA Method 29 Probe Wash ☐ EPA Method 202 Cup & Tube Wash

Job: Cyprus North Shore Source/Site: No 12 Rotocone - Stack North
Date Submitted: 1/16/95 Test No.: 6
Date of Analysis: 1/16/95 Technician: KT

Transport Leakage ☐ None ☒ ml Solvent: Acetone

Test: <u>6</u> Run: <u>0</u>	Dish No: <u>15</u>
Log No: <u>41664-416P</u>	Dish + Sample Wt: <u>49.9871</u> g
Volume of Solvent <u>120</u> ml	Dish Tare Wt: <u>49.9873</u> g
*Solvent Residue <u>1.67</u> ug/ml	Sample Wt: <u>0.0002</u> g
Test: <u>6</u> Run: <u>1</u>	Dish No: <u>17</u>
Vol. of Solvent <u>160</u> ml	Dish + Sample Wt: <u>48.3916</u> g
Log Number <u>-47P</u>	Dish Tare Wt: <u>48.4059</u> g
Comments	Sample Wt: <u>0.0143</u> g
Test: <u>6</u> Run: <u>2</u>	Dish No: <u>20</u>
Vol. of Solvent <u>100</u> ml	Dish + Sample Wt: <u>48.8135</u> g
Log Number <u>-48P</u>	Dish Tare Wt: <u>48.8254</u> g
Comments	Sample Wt: <u>0.0119</u> g
Test: <u>6</u> Run: <u>3</u>	Dish No: <u>22</u>
Vol. of Solvent <u>100</u> ml	Dish + Sample Wt: <u>51.3601</u> g
Log Number <u>-49P</u>	Dish Tare Wt: <u>51.3697</u> g
Comments	Sample Wt: <u>0.0096</u> g

*Solvent Residue 1.67 ug/ml = [(Sample Wt. 0.002 g) (10⁶)]/Vol. of Sol. 120 ml

EPA-M5 Acetone Residue Blank Spec. ≤ 7.8 ug/ml

	RUN 1	RUN 2	RUN 3	RUN
Results of Solvent Rinse g	<u>0.0140</u>	<u>0.0170-23</u>	<u>0.0094</u>	

EPA Method 5 Data Reporting Sheet Filter Gravimetrics

Job: Cypress North Shore Source: No 12 Rotocone
 Team Leader: GH Test Site: Stack North
 Date Submitted: 1/16/95 Date of Test: 1/10/95
 Test No.: 6 No. of Runs: 3
 Date of Analysis: _____ Technician: KT

Test:	6 Run: 0	Filter No:	7226
Field Blank:		Filter Type:	4"GF
Log No:	4664-46F	Filter Tare Wt:	0.9086 g
Comments:		Filter + Sample Wt:	0.9086 g
		Sample Wt:	0.0000 g
Test:	6 Run: 1	Filter No:	7114
Log No:	-0-47F	Filter Type:	4"GF
Comments:		Filter Tare Wt:	0.9423 g
		Filter + Sample Wt:	0.9436 g
		Sample Wt:	0.0013 g
Test:	6 Run: 2	Filter No:	7116
Log No:	-48F	Filter Type:	4"GF
Comments:		Filter Tare Wt:	0.9345 g
		Filter + Sample Wt:	0.9368 g
		Sample Wt:	0.0023 g
Test:	6 Run: 3	Filter No:	7118
Log No:	-49F	Filter Type:	4"GF
Comments:		Filter Tare Wt:	0.9490 g
		Filter + Sample Wt:	0.9526 g
		Sample Wt:	0.0036 g
Test:	Run:	Filter No:	
Log No:		Filter Type:	
Comments:		Filter Tare Wt:	g
		Filter + Sample Wt:	g
		Sample Wt:	g
Test:	Run:	Filter No:	
Log No:		Filter Type:	
Comments:		Filter Tare Wt:	g
		Filter + Sample Wt:	g
		Sample Wt:	g

Results:

Field Blank	Run 1	Run 2	Run 3	Run 4	Run 5
	0.0013	0.0023	0.0036		

Field Blk.	Run 1	Run 2	Run 3	Run 4	Run 5
	0.0158	0.0147	0.0136		

Impinger Catch Data Reporting Sheet

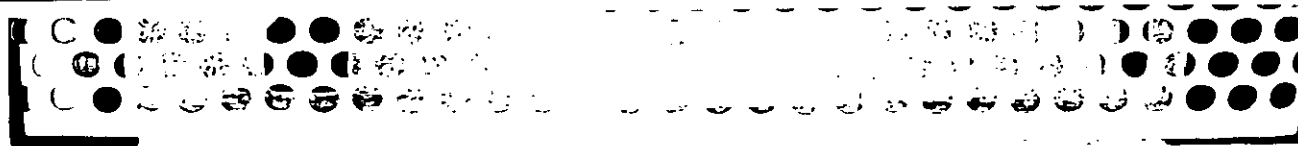
Protocol: ☒ Minnesota ☐ Wisconsin ☐ Iowa☐ EPA Method 202 ☐ OtherJob: Cypress North ShoreSource/Site: No. 2 Boiler/StackDate Submitted: 1-16-95Test No.: 7Date of Analysis: 1-20-95Technician: J. Lorenz

		Solvent Phase		Aqueous Phase	
Test: 7	Run: 0	Dish No: 15		Dish No:	
Log No: 4664-53 I		Dish + Sample Wt: 49.9865 g		Dish + Sample Wt:	
Color & Appearance:		Dish Tare Wt: 49.9861 g		Dish Tare Wt:	
		Fraction Wt: .0004 g		Fraction Wt:	
Comments: Field Blank		Smpl Vol: 500 ml, Alqt: 400 ml, Factor: 1.250		Smpl Vol: ml, Alqt: ml, Factor:	
		Sample Wt: .0005 g		Sample Wt:	
Test: 7	Run: 1	Dish No: 17		Dish No:	
Log No: -54 I		Dish + Sample Wt: 48.3910 g		Dish + Sample Wt:	
Color & Appearance:		Dish Tare Wt: 48.3898 g		Dish Tare Wt:	
		Fraction Wt: .0012 g		Fraction Wt:	
Comments:		Smpl Vol: 500 ml, Alqt: 400 ml, Factor: 1.250		Smpl Vol: ml, Alqt: ml, Factor:	
		Sample Wt: .0015 g		Sample Wt:	
Test: 7	Run: 2	Dish No: 20		Dish No:	
Log No: -55 I		Dish + Sample Wt: 48.8150 g		Dish + Sample Wt:	
Color & Appearance:		Dish Tare Wt: 48.8129 g		Dish Tare Wt:	
		Fraction Wt: .0021 g		Fraction Wt:	
Comments:		Smpl Vol: 500 ml, Alqt: 400 ml, Factor: 1.250		Smpl Vol: ml, Alqt: ml, Factor:	
		Sample Wt: .0026 g		Sample Wt:	
Test: 7	Run: 3	Dish No: 59		Dish No:	
Log No: -56 I		Dish + Sample Wt: 44.7352 g		Dish + Sample Wt:	
Color & Appearance:		Dish Tare Wt: 44.7337 g		Dish Tare Wt:	
		Fraction Wt: .0015 g		Fraction Wt:	
Comments:		Smpl Vol: 500 ml, Alqt: 400 ml, Factor: 1.250		Smpl Vol: ml, Alqt: ml, Factor:	
		Sample Wt: .0019 g		Sample Wt:	

Note: Factor = Sample Volume/Aliquot Volume

Blank Solvent Wt. .0001 g

	RUN Field Blank 0	RUN 1	RUN 2	RUN 3
Results of Solvent Phase	.0005	.0010	.0021	.0014
Results of Aqueous Phase		D-25		



EPA Method 5 Data Reporting Sheet Probe/Cyclone Wash

Job <u>Cypress North Shore</u>	Source <u>No 2 Boiler</u>
Team Leader <u>DUH</u>	Test Site <u>STICK</u>
Date Submitted <u>1/16/95</u>	Date of Test <u>1/12/95</u>
Test No. <u>7</u>	No. of Runs <u>3</u>
Date of Analysis <u>1/16/95</u>	Technician <u>KT</u>
Transport Leakage ☐ <u>None</u> ml	Solvent <u>Acetone</u>

Test: <u>7</u> Run: <u>0</u>	Dish No: <u>23</u>
Field Blank: <u>130</u>	Dish Tare Wt: <u>46.0853</u> g
Log No: <u>4664-53P</u>	Dish + Sample Wt: <u>46.0858</u> g
Volume of Solvent <u>100</u> ml	Sample Wt: <u>0.0005</u> g
*Solvent Residue <u>5.0</u> ug/ml	
Test: <u>7</u> Run: <u>1</u>	Dish No: <u>32</u>
Vol. of Solvent <u>150</u> ml	Dish Tare Wt: <u>57.8077</u> g
Log Number <u>-54P</u>	Dish + Sample Wt: <u>57.8338</u> g
Comments	Sample Wt: <u>0.0261</u> g
Test: <u>7</u> Run: <u>2</u>	Dish No: <u>39</u>
Vol. of Solvent <u>140</u> ml	Dish Tare Wt: <u>49.4371</u> g
Log Number <u>-55P</u>	Dish + Sample Wt: <u>49.4574</u> g
Comments	Sample Wt: <u>0.0203</u> g
Test: <u>7</u> Run: <u>3</u>	Dish No: <u>52</u>
Vol. of Solvent <u>160</u> ml	Dish Tare Wt: <u>50.8901</u> g
Log Number <u>-56P</u>	Dish + Sample Wt: <u>50.9118</u> g
Comments	Sample Wt: <u>0.0217</u> g
Test: Run:	Dish No:
Log No:	Dish Tare Wt: g
Comments:	Dish + Sample Wt: g
	Sample Wt: g
Test: Run:	Dish No:
Vol of Solvent ml	Dish Tare Wt: g
Log Number	Dish + Sample Wt: g
Comments	Sample Wt: g

*Solvent Residue 5.0 ug/ml = [(Sample Wt. 0.005 g) (10⁶)] / Vol. of Sol. 100 ml

EPA-M5 Acetone Residue Blank Spec. ≤ 7.8 ug/ml

Results:

Blank Solvent Wt. _____

Field Blank	Run 1	Run 2	Run 3	Run 4	Run 5
	<u>0.0253</u>	<u>0.0196</u>	<u>0.0209</u>	<u>D-26</u>	

EPA Method 5 Data Reporting Sheet

Source: Cyprus North Shore No. 2 Boiler
 Test Site: DVH Stack
 Date of Test: 1/16/95 1/12/95
 No. of Runs: 7 3
 Technician: 1/16/95 KT

7 Run: 0	Filter No:	7071
Rank:	Filter Type:	4" GF
4664-53F	Filter Tare Wt:	0.9534 g
Comments:	Filter + Sample Wt:	0.9534 g
	Sample Wt:	0.0000 g
7 Run: 1	Filter No:	7053
No: -54F	Filter Type:	4" GF
Comments:	Filter Tare Wt:	0.9684 g
	Filter + Sample Wt:	0.9763 g
	Sample Wt:	0.0079 g
7 Run: 2	Filter No:	7073
No: -55F	Filter Type:	4" GF
Comments:	Filter Tare Wt:	0.9547 g
	Filter + Sample Wt:	0.9628 g
	Sample Wt:	0.0081 g
7 Run: 3	Filter No:	7099
Log No: -56F	Filter Type:	4" GF
Comments:	Filter Tare Wt:	0.9446 g
	Filter + Sample Wt:	0.9543 g
	Sample Wt:	0.0097 g
Test: Run:	Filter No:	
Log No:	Filter Type:	
Comments:	Filter Tare Wt:	g
	Filter + Sample Wt:	g
	Sample Wt:	g
Test: Run:	Filter No:	
Log No:	Filter Type:	
Comments:	Filter Tare Wt:	g
	Filter + Sample Wt:	g
	Sample Wt:	g

Results:

Field Blank	Run 1	Run 2	Run 3	Run 4	Run 5
	0.0079	0.0081	0.0097		

Field Blk.	Run 1	Run 2	Run 3	Run 4	Run 5
	0.0342	0.0298	0.0320		

EPA Method 5 Data Reporting Sheet Probe/Cyclone Wash

Job <u>Cypress North Shore</u> Team Leader <u>GH</u> Date Submitted <u>1/16/95</u> Test No. <u>8</u> Date of Analysis <u>1/16/95</u> Transport Leakage ☒ None <u>5</u> ml	Source <u>No 101 Fine Crushed</u> Test Site <u>Stack</u> Date of Test <u>1/13/95</u> No. of Runs <u>3</u> Technician <u>KT</u> Solvent <u>Acetone</u>
--	--

Test: <u>8</u> Run: <u>0</u> Field Blank: Log No: <u>4664-60P</u> Volume of Solvent <u>140</u> ml *Solvent Residue <u>1.43</u> ug/ml	Dish No: <u>53</u> Dish Tare Wt: <u>47.4077</u> g Dish + Sample Wt: <u>47.4079</u> g Sample Wt: <u>0.0002</u> g
Test: <u>8</u> Run: <u>1</u> Vol. of Solvent <u>120</u> ml Log Number <u>-61P</u> Comments	Dish No: <u>98</u> Dish Tare Wt: <u>47.2115</u> g Dish + Sample Wt: <u>47.2319</u> g Sample Wt: <u>0.0204</u> g
Test: <u>8</u> Run: <u>2</u> Vol. of Solvent <u>140</u> ml Log Number <u>-62P</u> Comments	Dish No: <u>104</u> Dish Tare Wt: <u>44.7555</u> g Dish + Sample Wt: <u>44.7709</u> g Sample Wt: <u>0.0154</u> g
Test: <u>8</u> Run: <u>3</u> Vol. of Solvent <u>140</u> ml Log Number <u>-63P</u> Comments	Dish No: <u>204</u> Dish Tare Wt: <u>47.4687</u> g Dish + Sample Wt: <u>47.4764</u> g Sample Wt: <u>0.0077</u> g
Test: Run: Log No: Comments:	Dish No: Dish Tare Wt: Dish + Sample Wt: Sample Wt:
Test: Run: Vol of Solvent ml Log Number Comments	Dish No: Dish Tare Wt: Dish + Sample Wt: Sample Wt:

*Solvent Residue 1.43 ug/ml = [(Sample Wt 0.0002g) (10⁶)]/Vol. of Sol. 140 ml

EPA-M5 Acetone Residue Blank Spec. ≤ 7.8 ug/ml

Results:

Blank Solvent Wt.

Field Blank	Run 1	Run 2	Run 3	Run 4	Run 5
	<u>0.0202</u>	<u>0.0152</u>	<u>0.0075</u>	<u>D-29</u>	

EPA Method 5 Data Reporting Sheet Filter Gravimetrics

Job: <u>Cypress North Shore</u>	Source: <u>No 101 Fine Cusher</u>
Team Leader: <u>GH</u>	Test Site: <u>Stack</u>
Date Submitted: <u>1/16/95</u>	Date of Test: <u>1/13/95</u>
Test No.: <u>8</u>	No. of Runs: <u>3</u>
Date of Analysis: _____	Technician: <u>KT</u>

Test: <u>8</u> Run: <u>0</u>	Filter No: <u>7141</u>
Field Blank:	Filter Type: <u>4"GF</u>
Log No: <u>4664-60F</u>	Filter Tare Wt: <u>0.9460</u> g
Comments:	Filter + Sample Wt: <u>0.9461</u> g
	Sample Wt: <u>0.0001</u> g
Test: <u>8</u> Run: <u>1</u>	Filter No: <u>7120</u>
Log No: <u>-61F</u>	Filter Type: <u>4"GF</u>
Comments:	Filter Tare Wt: <u>0.9471</u> g
	Filter + Sample Wt: <u>0.9485</u> g
	Sample Wt: <u>0.0014</u> g
Test: <u>8</u> Run: <u>2</u>	Filter No: <u>7119</u>
Log No: <u>-62F</u>	Filter Type: <u>4"GF</u>
Comments:	Filter Tare Wt: <u>0.9545</u> g
	Filter + Sample Wt: <u>0.9548</u> g
	Sample Wt: <u>0.0003</u> g
Test: <u>8</u> Run: <u>3</u>	Filter No: <u>7117</u>
Log No: <u>-63F</u>	Filter Type: <u>4"GF</u>
Comments:	Filter Tare Wt: <u>0.9569</u> g
	Filter + Sample Wt: <u>0.9575</u> g
	Sample Wt: <u>0.0006</u> g
Test: _____ Run: _____	Filter No: _____
Log No: _____	Filter Type: _____
Comments:	Filter Tare Wt: _____ g
	Filter + Sample Wt: _____ g
	Sample Wt: _____ g
Test: _____ Run: _____	Filter No: _____
Log No: _____	Filter Type: _____
Comments:	Filter Tare Wt: _____ g
	Filter + Sample Wt: _____ g
	Sample Wt: _____ g

Results:

Field Blank	Run 1	Run 2	Run 3	Run 4	Run 5
	<u>0.0014</u>	<u>0.0003</u>	<u>0.0006</u>		

Field Blk.	Run 1	Run 2	Run 3	Run 4	Run 5
	<u>0.0233</u>	<u>0.0173</u>	<u>0.0094</u>		

Impinger Catch Data Reporting Sheet

Protocol: ☒ Minnesota ☐ Wisconsin ☐ Iowa
Job: Cypress North Shore
Date Submitted: 1-16-95
Date of Analysis: 1-20-95

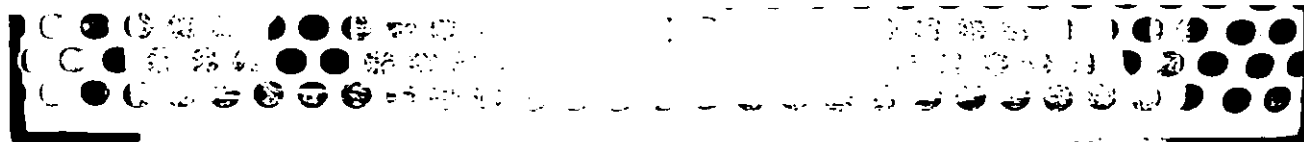
☐ EPA Method 202 ☐ Other _____
Source/Site: Dry Cobber / stack
Test No.: 9
Technician: J. Lorenz

		Solvent Phase		Aqueous Phase	
Test: 9	Run: 0	Dish No: 739		Dish No:	
Log No: 4664-64I		Dish + Sample Wt: 45.3591 g		Dish + Sample Wt:	
Color & Appearance:		Dish Tare Wt: 45.3587 g		Dish Tare Wt:	
		Fraction Wt: .0004 g		Fraction Wt:	
Comments: Field Blank		Smpl Vol: ml, Alqt: ml, Factor: 1.000		Smpl Vol: ml, Alqt: ml, Factor:	
		Sample Wt: .0004 g		Sample Wt:	
Test: 9	Run: 1	Dish No: 740		Dish No:	
Log No: -65I		Dish + Sample Wt: 44.9529 g		Dish + Sample Wt:	
Color & Appearance:		Dish Tare Wt: 44.9520 g		Dish Tare Wt:	
		Fraction Wt: .0009 g		Fraction Wt:	
Comments:		Smpl Vol: ml, Alqt: ml, Factor: 1.000		Smpl Vol: ml, Alqt: ml, Factor:	
		Sample Wt: .0009 g		Sample Wt:	
Test: 9	Run: 2	Dish No: 741		Dish No:	
Log No: -66I		Dish + Sample Wt: 42.3810 g		Dish + Sample Wt:	
Color & Appearance:		Dish Tare Wt: 42.3799 g		Dish Tare Wt:	
		Fraction Wt: .0011 g		Fraction Wt:	
Comments:		Smpl Vol: ml, Alqt: ml, Factor: 1.000		Smpl Vol: ml, Alqt: ml, Factor:	
		Sample Wt: .0011 g		Sample Wt:	
Test: 9	Run: 3	Dish No: 744		Dish No:	
Log No: -67I		Dish + Sample Wt: 48.6345 g		Dish + Sample Wt:	
Color & Appearance:		Dish Tare Wt: 48.6341 g		Dish Tare Wt:	
		Fraction Wt: .0004 g		Fraction Wt:	
Comments:		Smpl Vol: ml, Alqt: ml, Factor: 1.000		Smpl Vol: ml, Alqt: ml, Factor:	
		Sample Wt: .0004 g		Sample Wt:	

Note: Factor = Sample Volume/Aliquot Volume

Blank Solvent Wt: .0001 g

	RUN 0 Field Blank	RUN 1	RUN 2	RUN 3
Results of Solvent Phase	.0004	.0005	.0007	.0000
Results of Aqueous Phase	D-31			



EPA Method 5 Data Reporting Sheet Probe/Cyclone Wash

Job <u>Cypus North Shore</u>	Source <u>Dug Clobber</u>
Team Leader <u>DVH</u>	Test Site <u>Stack</u>
Date Submitted <u>1/16/95</u>	Date of Test <u>1/13/95</u>
Test No. <u>9</u>	No. of Runs <u>3</u>
Date of Analysis <u>1/16/95</u>	Technician <u>KT</u>
Transport Leakage ☐ <u>None</u> ml	Solvent <u>Acetone</u>

Test: <u>9</u> Run: <u>0</u>	Dish No: <u>306</u>
Field Blank:	Dish Tare Wt: <u>42.8337</u> g
Log No: <u>4664-64P</u>	Dish + Sample Wt: <u>42.8341</u> g
Volume of Solvent <u>150</u> ml	Sample Wt: <u>0.0004</u> g
*Solvent Residue <u>2.67</u> ug/ml	
Test: <u>9</u> Run: <u>1</u>	Dish No: <u>311</u>
Vol. of Solvent <u>70</u> ml	Dish Tare Wt: <u>43.8108</u> g
Log Number <u>-65P</u>	Dish + Sample Wt: <u>43.8239</u> g
Comments	Sample Wt: <u>0.0131</u> g
Test: <u>9</u> Run: <u>2</u>	Dish No: <u>324</u>
Vol. of Solvent <u>90</u> ml	Dish Tare Wt: <u>46.2159</u> g
Log Number <u>-66P</u>	Dish + Sample Wt: <u>46.2262</u> g
Comments	Sample Wt: <u>0.0103</u> g
Test: <u>9</u> Run: <u>3</u>	Dish No: <u>326</u>
Vol. of Solvent <u>100</u> ml	Dish Tare Wt: <u>43.4733</u> g
Log Number <u>-67P</u>	Dish + Sample Wt: <u>43.4796</u> g
Comments	Sample Wt: <u>0.0063</u> g
Test: Run:	Dish No:
Log No:	Dish Tare Wt: g
Comments:	Dish + Sample Wt: g
	Sample Wt: g
Test: Run:	Dish No:
Vol of Solvent ml	Dish Tare Wt: g
Log Number	Dish + Sample Wt: g
Comments	Sample Wt: g

*Solvent Residue 2.67 ug/ml = [(Sample Wt. 0.0004 g) (10⁶)]/Vol. of Sol. 150 ml

EPA-M5 Acetone Residue Blank Spec. ≤ 7.8 ug/ml

Results:

Blank Solvent Wt. _____

Field Blank	Run 1	Run 2	Run 3	Run 4	Run 5
	<u>0.0129</u>	<u>0.0101</u>	<u>0.0060</u>	<u>D-32</u>	

EPA Method 5 Data Reporting Sheet Filter Gravimetrics

Job: Cyprus North Shore Source: Dry Cobber
 Team Leader: DVH Test Site: Stack
 Date Submitted: 8/1/16/95 Date of Test: 1/13/95
 Test No.: 9 No. of Runs: 3
 Date of Analysis: 1/16/95 Technician: KT

Test: <u>9</u> Run: <u>0</u>	Filter No: <u>7069</u>
Field Blank:	Filter Type: <u>4"GF</u>
Log No: <u>4664-64F</u>	Filter Tare Wt: <u>0.9416</u> g
Comments:	Filter + Sample Wt: <u>0.9420</u> g
	Sample Wt: <u>0.0004</u> g
Test: <u>9</u> Run: <u>1</u>	Filter No: <u>6763</u>
Log No: <u>-66F</u>	Filter Type: <u>4"GF</u>
Comments:	Filter Tare Wt: <u>0.94162</u> g
	Filter + Sample Wt: <u>0.9480</u> g
	Sample Wt: <u>0.0018</u> g
Test: <u>9</u> Run: <u>2</u>	Filter No: <u>6762</u>
Log No: <u>-66F</u>	Filter Type: <u>4"GF</u>
Comments:	Filter Tare Wt: <u>0.9500</u> g
	Filter + Sample Wt: <u>0.9508</u> g
	Sample Wt: <u>0.0008</u> g
Test: <u>9</u> Run: <u>3</u>	Filter No: <u>7070</u>
Log No: <u>-67F</u>	Filter Type: <u>4"GF</u>
Comments:	Filter Tare Wt: <u>0.9417</u> g
	Filter + Sample Wt: <u>0.9420</u> g
	Sample Wt: <u>0.0003</u> g
Test: Run:	Filter No:
Log No:	Filter Type:
Comments:	Filter Tare Wt: g
	Filter + Sample Wt: g
	Sample Wt: g
Test: Run:	Filter No:
Log No:	Filter Type:
Comments:	Filter Tare Wt: g
	Filter + Sample Wt: g
	Sample Wt: g

Results:

Field Blank	Run 1	Run 2	Run 3	Run 4	Run 5
	<u>0.0018</u>	<u>0.0008</u>	<u>0.0003</u>		

Field Blk.	Run 1	Run 2	Run 3	Run 4	Run 5
	<u>0.0152</u>	<u>0.0114</u>	<u>0.0063</u>		

0.0116 SAB 130

EPA Method 6 Sulfur Dioxide Calculation Data Sheet¹

Job	<u>Cypress Northshore Mining</u>	Source	<u>No. 1205 Waste Gas</u>
Team Leader	<u>J.S.</u>	Test Site	<u>Stack</u>
Date Submitted	<u>1-16-95</u>	Date Of Test	<u>1-11-95</u>
Test No.	<u>4</u>	No. Of Runs Completed	<u>3</u>
Date Of Analysis	<u>1-17-95</u>	Technician	<u>B. J. Dele</u>

MEQ Calculation:

$$MEQ = \frac{DF \cdot N \cdot (V_t - V_b) \cdot V_{soln}}{V_a}$$

DF = Dilution Factor
N = Normality Of Titrant
V_t = Volume Of Titrant Used in Sample (ml)
V_b = Volume Of Titrant Used in Blank (ml)
V_{soln} = Total Volume Of Sample (ml)
V_a = Volume Of Aliquot (ml)

Water Catch:

Test 4 Run 1 MEQ = $\frac{(1.0)(0.0100)(0.40 - 0.15)(510)}{(20.0)} = 0.064$ MEQ

Test 4 Run 2 MEQ = $\frac{(1.0)(0.0100)(0.40 - 0.15)(510)}{(20.0)} = 0.064$ MEQ

Test 4 Run 3 MEQ = $\frac{(1.0)(0.0100)(0.60 - 0.15)(510)}{(20.0)} = 0.115$ MEQ

3% Peroxide Catch:

Test 4 Run 1 MEQ = $\frac{(1.0)(0.0100)(0.40 - 0.15)(500)}{(20.0)} = 0.063$ MEQ

Test 4 Run 2 MEQ = $\frac{(1.0)(0.0100)(0.30 - 0.15)(500)}{(20.0)} = 0.038$ MEQ

Test 4 Run 3 MEQ = $\frac{(1.0)(0.0100)(0.30 - 0.15)(500)}{(20.0)} = 0.038$ MEQ

Total MEQ Per Run:

Test 4 Run 1 = 0.127 MEQ

Test 4 Run 2 = 0.102 MEQ

Test 4 Run 3 = 0.153 MEQ

Comments _____

¹ Form to be used in conjunction with combination method 5 and 6 train.

Interpoll Laboratories
(612)786-6020

EPA Method 7A Recovery and Analysis Data Sheet (1)

*****SOURCE*****
Job Cyperus Northshore Mining
Source No. 1205 Waste Gas Stack
Date of Sampling 1-11-95
Test No(s) 4
*****RECOVERY*****
Date of Recovery 1-18-95
Recovery volume 500 ml
Barometric at time 29.24 IN.HG.
*****ANALYTICAL*****
Date of Analysis 2/8/95
Analyst TPW
Eluent AS4A
Chromatograph: Dionex System 4000i

Samples collected in accordance with EPA Method 7, CFR Title 40, Part 60, Appendix A. Samples analyzed in accordance with EPA Method 7A by ion chromatography. Mercury manometers used to measure flask pressures/vacuums in sampling and in recovery. Thommen Model TX 19 jewel barometer calibrated against laboratory mercury in glass barometer used to measure field barometric pressure. Three field blanks are prepared and the average used to correct measured nitrate concentrations. All samples are analyzed as a batch using a Dionex Model 4270 Chromatograph Data Integrator. The integrator is programmed to give the actual concentration of the 500 ml recovered sample even if a subsequent dilution was made. The dilution indicated here as well as on the chromatogram.

$$C_{RS} = DF(C_{DS}) \quad M_{NO_3} = (C_{RS} - \bar{C}_B)V_R \quad \bar{C}_B = (C_{B1} + C_{B2} + C_{B3})/3$$

where: C_{RS} = concentration of nitrate in 500 ml recovered sample in ug/ml

DF = dilution factor

C_{DS} = concentration of nitrate of a 500 ml recovered sample which has been diluted by a factor of DF to bring it into the proper range for the ion chromatograph. This value is an intermediate number and is not outputted by the electronic integrator which is programmed to output the concentration of the original undiluted 500 ml recovered sample.

M_{NO_3} = total mass of nitrate in micrograms in the 500 ml recovered sample and/or in the 2L flask.

C_B = average conc. of nitrate in 500 ml recovered samples from the three field blanks (ug/ml)

C_{B1}, C_{B2}, C_{B3} = conc. of nitrate in 500 ml recovered samples from the three field blanks (ug/ml)

V_R = recovery volume for samples and field blanks in ml

(612) 786-6020

Sample Chain of Custody

Source

Source

Site 5:W 5701234-2

2024.5

Log No.

Log No.

Job

Field Engineer

Date of Test

Test 1-10-95

No. of R

No. of Runs

Field

No. Items	Sample Type	Analyst	Sequence No.	Comments
4	Probe Wash: ☒ Acetone ☐ MeCl ₃	☒ EPA M-5 ☐ EPA M-29		
4	Filter: ☒ 4" Glass ☐ 55 Thimble	☒ EPA M-5 ☐ EPA M-29 ☐ EPA M-201A		
4	Impingers: ☒ DI Water ☐ 3% H ₂ O ₂ ☐ 1N NaOH ☐ 2,4-DNPH	☒ MIN Protocol ☐ W/1 Protocol ☐ EPA M-202 ☐ EPA M6,8 ☐ Acid Cases		
1	Integrated Gas: ☐ Tedlar Bag	☐ EPA M-3 ☐ _____		
	Oxides of Nitrogen:	☐ EPA M-7A ☐ _____		
	Fuel Lab: ☐ Fuel Sample	☐ Per S-0163		
	Particle Sizing:	☐ X-Ray Scdgraph ☐ _____		
	Miscellaneous:	☐ _____		

Coal	Tuna	Coal	☐ Bituminous	Wood	☐ Wood Waste	Oil	☐ Waste Oil	Misc	☐ Natural Gas
------	------	------	-------------------------------------	------	-------------------------------------	-----	------------------------------------	------	--------------------------------------

Misc: ☐ Natural Gas

☐ Natural Gas☐ Natural Gas

Relinquished by/Affiliation

Accepted by/Affiliation

Date _____

E. T. Munnings - water pump	OK	water pump	1/10/95	0830

INTERPOIL LABORATORIES, INC.

(612) 786-6020

Sample Chain of Custody

Cyprus N. Shawa Source

1104 PEA-MER

Site

Test No.

3

Log No.

No. of Runs

4664

3

Job Field Engineer

G. HOYE

Date of Test

1-9-95

No. Items	Sample Type	Analysis	Sequence No.	Comments
4	Probe Wash: ☒ Acetone ☐ MeCl ₃	☒ EPA M-5 ☐ EPA M-29		
4	Filter: ☒ 4" Glass ☐ SS Thimble	☒ EPA M-5 ☐ EPA M-29 ☐ EPA M-201A		
4	Impingers: ☒ DI Water ☐ 3% I ₂ O ₂ ☐ 1N NaOH ☐ 2,4-DNPH	☒ IIA Protocol ☐ IWI Protocol ☐ EPA M-202 ☐ EPA M-6,8 ☐ Acid Gases		
3	Integrated Gas: ☒ Tedlar Bag	☒ EPA M-3		
0	Oxides of Nitrogen:	☐ EPA M-7A		
0	Fuel Lab: ☐ Fuel Sample	☐ Per S-0163		
0	Particle Sizing:	☐ X-Ray Sdgraph ☐ Cascade Imp		
	Miscellaneous:	☐		

Misc: ☐ Natural Gas
☐ RDF
☐

Oil: ☐ Waste Oil
☐ No. 2
☐ No. 6

Wood: ☐ Wood Waste
☐ Dust
☐ Bark

Fuel Type: Coal: ☐ Bituminous
☐ Anthracite
☐ Lignite

Relinquished by/Affiliation

Accepted by/Affiliation

Date

Gary Hove / stub

Carl Interpoll

1/10/95 0830

INTERPOIL LABORATORIES, INC.
(612) 786-6020

Sample Chain of Custody

Job CYPRUS N Shore Source DATE

Field Engineer GAH Date of Test 12/12/95

Site NO 12 FELLTZERS Log No.
Test No. ROTACATE STACK No. of Runs

4667

3

No. Items	Sample Type	Analysis	Sequence No.	Comments
3	Probe Wash: ☒ Acetone ☐ MeCl ₂	☒ EPA M-5 ☐ EPA M-29	☐ EPA M-201A ☐ _____	
3	Filter: ☒ 4" Glass ☐ SS Thimble	☒ EPA M-5 ☐ EPA M-29 ☐ EPA M-201A	☐ EPA M-17	
3	Impingers: ☒ DI Water ☐ 3% H ₂ O ₂ ☐ 1N NaOH ☐ 2,4-DNPH	☒ MIN Protocol ☐ Wt Protocol ☐ EPA M-202 ☐ EPA M-6,8 ☐ Acid Gases	☐ JIA Protocol ☐ Formaldehyde ☐ EPA M-29 ☐ EPA M-26 ☐ _____	
3	Integrated Gas: ☒ Tedlar Bag	☒ EPA M-3 ☐ _____	☐ EPA M-10	
0	Oxides of Nitrogen:	☐ EPA M-7A ☐ _____		
0	Fuel Lab: ☐ Fuel Sample	☐ Per S-0163		
0	Particle Sizing:	☐ X-Ray Sdgraph ☐ _____	☐ Cascade Imp	
0	Miscellaneous: ☐ _____	☐ _____		

☐ Natural Gas
☐ TRDF
☐ _____

Misc:
☐ _____

Oil:
☐ Waste Oil
☐ No. 2
☐ No. 6

Wood: ☐ Wood Waste
☐ Dust
☐ Bark

Fuel Type: Coal: ☐ Bituminous
☐ Anthracite
☐ Lignite

Accepted by/Affiliation

Date

Relinquished by/Affiliation

GAH / Interpol

1/10/95 0830

033094-GASTACKWFORMSIS-278.2

INTERPOL LABORATORIES, INC.
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Sample Chain of Custody

Log No. 4664
No. of Runs 3

Job Cypress Northgate
Field Engineer J.S.

Source Becker Site
Date of Test 1/12/95

Test No. 7

No. Items	Sample Type	Analysis	Sequence No.	Comments
4	Probe Wash: ☒ Acetone ☐ MeCl ₂	☐ DI Water ☐ _____	☒ EPA M-5 ☐ EPA M-29	☐ EPA M-201A ☐ _____
4	Filter: ☒ 4" Glass ☐ 55 Thimble	☐ Pallflex ☐ 2.5" Glass	☒ EPA M-5 ☐ EPA M-29 ☐ EPA M-201A	☐ EPA M-17
4	Injurers: ☒ DI Water ☒ 3% H ₂ O ₂ ☐ 1N NaOH ☐ 2,4-DNPH	☐ H ₂ SO ₄ ☐ HNO ₃ /H ₂ O ₂ ☐ KMnO ₄ /H ₂ SO ₄ ☐ _____	☒ MIN Protocol ☐ IWI Protocol ☐ EPA M-202 ☒ EPA M-6,8 ☐ Acid Gases	☐ IIA Protocol ☐ Formaldehyde ☐ EPA M-29 ☐ EPA M-26 ☐ _____
3	Integrated Gas: ☐ Tedlar Bag	☐ _____	☐ EPA M-3 ☐ _____	☐ EPA M-10
	Oxides of Nitrogen:		☐ EPA M-7A ☐ _____	
	Fuel Lab: ☐ Fuel Sample	☐ Aggregate	☐ Per S-0163	
	Particle Sizing:		☐ X-Ray Sdgraph ☐ _____	☐ Cascade Imp
	Miscellaneous:	☐ _____	☐ _____	

Fuel Type: Coal: ☐ Bituminous ☐ Anthracite ☐ Lignite
Oil: ☐ Waste Oil ☐ No. 2 ☐ No. 6
Misc: ☐ Natural Gas ☐ RDF ☐ _____

Relinquished by/Affiliation	Accepted by/Affiliation	Date
<u>Jeff Anzola</u>	<u>SGD Interpol</u>	<u>1/12/95</u>
		<u>1/16/95 6830</u>

INTERPOLL LABORATORIES, INC.

(612) 786-6020

Sample Chain of Custody

Job: Cypress North Shore Source Date of Test: 1/13/95 Test No.: 9 Log No.: 4664
 Field Engineer: Drew No. of Runs: 3

No. Items	Sample Type	Analysis	Sequence No.	Comments
41	Probe Wash: ☒ Acetone ☐ MeCl ₃	☒ EPA M-5 ☐ EPA M-29		
41	Filter: ☒ 4" Glass ☐ 55 Thimble	☒ EPA M-5 ☐ EPA M-29 ☐ EPA M-201A		
41	Impingers: ☒ DI Water ☐ 3% H ₂ O ₂ ☐ 1N NaOH ☐ 2,4-DNPH	☒ EPA M-5 ☐ EPA M-29 ☐ EPA M-201A ☐ EPA M-17		
41	Integrated Gas: ☐ Tedlar Bag	☐ EPA M-3 ☐ EPA M-10		
	Oxides of Nitrogen:	☐ EPA M-7A ☐ EPA M-7B		
	Fuel Lab: ☐ Fuel Sample	☐ Per S-0163		
	Particle Sizing:	☐ X-Ray Scigraph ☐ Cascade Imp		
	Miscellaneous:	☐		

Fuel Type: Coal: ☐ Bituminous ☐ Anthracite ☐ Lignite
 Wood: ☐ Wood Waste ☐ Dust ☐ Bark
 Oil: ☐ Waste Oil ☐ No. 2 ☐ No. 6
 Misc: ☐ Natural Gas ☐ RDF ☐

Relinquished by/Affiliation	Accepted by/Affiliation	Date
<u>Drew Van Hoover</u>	<u>CLD / inter poll</u>	<u>1/13/95</u>
		<u>1/14/95 0830</u>

APPENDIX E

REQUIRED DATA FOR COMBUSTION SOURCES

(Not Available at Time of Report Publication)

APPENDIX F

OPERATIONAL DATA

(Not Available at Time of Report Publication)

APPENDIX G

PROCEDURES

Particulate Loading and Emission Rates

The particulate emission rates were determined per EPA Methods 1 - 5, CFR Title 40, Part 60, Appendix A (revised July 1, 1992). In this procedure a preliminary velocity profile of the gases in the flue is obtained by means of a temperature and velocity traverse. On the basis of these values, sampling nozzles of appropriate diameter are selected to allow isokinetic sampling, a necessary prerequisite for obtaining a representative sample.

The sampling train consists of a heated glass-lined sampling probe equipped with a Type S pitot and a thermocouple. The probe is attached to a sampling module which houses the all-glass in line filter holder in a temperature controlled oven. The sampling module also houses the impinger case and a Drierite filled column. The sampling module is connected by means of an umbilical cord to the control module. The control module houses the dry test gas meter, the calibrated orifice, a leakless pump, two inclined manometers, and all controls required for operating the sampling train.

Particulate samples are collected as follows: The sample gas is drawn through the sampling probe isokinetically and passed through a 4-inch diameter Gelman Type A/E glass fiber filter where particulates are removed. The sample gas is then passed through an ice-cooled impinger train and a desiccant-packed column which absorbs remaining moisture. The sample gas then passes through a vacuum pump followed by a dry test gas meter. The gas meter integrates the sample gas flow throughout the course of the test. A calibrated orifice attached to the outlet of the gasmeter provides real time flow rate data.

A representative particulate sample was acquired by sampling for equal periods of time at the centroid of a number of equal area regions in the duct. The sampling rate is adjusted at each test point maintaining isokinetic sampling conditions. Nomographs are used for rapid determination of the sampling rate.

Particulate Loading and Emission Rates

After sampling is complete, the filter is removed and placed in a clean container. The nozzle and inlet side of the filter holder are quantitatively washed with acetone and the washings are stored in a second container. A brush is often used in the cleaning step to help dislodge deposits. The samples are returned to the laboratory where they are logged in and analyzed. The volume of the acetone rinse ("probe wash") is noted and then the rinse is quantitatively transferred to a tared 120 cc porcelain evaporating dish and the acetone evaporated off at 97-105 °F. This temperature is used to prevent condensation of atmospheric moisture due to the cooling effect induced by the evaporation of acetone. The acetone-free sample is then transferred to an oven and dried at 105 °C for 30 minutes, cooled in a desiccator over Drierite, and then weighed to the nearest .01 mg. The filter sample is quantitatively transferred to a 6-inch watch glass and dried in an oven at 105 °C for two hours. The filter and watch glass are then cooled in a desiccator and the filter weighed to the nearest .01 mg. All weighings are performed in a balance room where the relative humidity is hydrostatted to less than 50% relative humidity. Microscopic examination of the samples is performed if any unusual characteristics are observed. The weight of the acetone rinse is corrected for the acetone blank. The Drierite column is weighed on-site and the water collected by Drierite is added to the condensate so that the total amount of absorbed water may be ascertained.

Integrated flue gas samples for Orsat analysis were collected simultaneously with each pollutant sample. The samples were collected in 15-liter gas sampling bags at a constant flow rate throughout each particulate run. The bags were at a constant flow rate throughout each particulate run. The bags were then returned to the laboratory and analyzed by Orsat analysis. Standard commercially prepared solutions were used in the Orsat analyzer (sat. KOH for carbon dioxide and reduced methylene blue for oxygen).

Condensable Organic Compounds Analysis

(State of Minnesota - MPCA Exhibit C)

Method II-8672-MN

Equipment: Separatory funnel - 500 cc with Teflon stopcock

 Powder funnel - 75 mm ID with a 17 mm stem

 Evaporating dish(es) - 200 cc or 250 cc beaker

Reagents: Diethyl ether - reagent grade

 Chloroform - reagent grade

 Sodium sulfate - (ACS) granular anhydrous

 Toluene - (if 3% hydrogen peroxide is used to collect the samples)

 Glass wool (Pyrex microfiber)

PREPARATION

1. Place 1 kg of granular anhydrous sodium sulfate in a shallow tray and heat to 200°C for at least four hours. Store in a tightly sealed glass container.
2. Place a plug of clean glass wool in the stem of the powder funnel. The plug must be of sufficient size so that it is held snugly in place by its own pressure. Add a one-inch layer of dry sodium sulfate.

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SAMPLING

An all-glass impinger assembly is used in the back half of the EPA Method 5 sampling train when an organic wet catch is to be collected. The impinger assembly consists of a modified impinger, a Greenburg Smith impinger followed by another modified impinger. The third impinger should have a temperature measuring device at the outlet upstream of a *final impinger* or desiccant column to monitor the temperature of the outlet gas stream. Prior to the start of the test, each of the first two impingers should be charged with 100 g of Class I water. The Method 5 train should be operated as provided for in EPA Method 5. Ice should be added to the impinger bath to keep the temperature of the gas at the outlet at or less than 68°F. After the post test leak check, the impinger train is removed and impinger contents poured into a tared all-glass sample bottle and closed with a Teflon-lined cap. The sample bottle is then weighed and the total condensate calculated by subtraction of the bottle tare weight and the weight of initial water added to the impingers (200 g). A label is affixed and the sample is returned to the laboratory for analysis. The sample should be stored at 4°C if the analysis is not conducted within 48 hours.

ANALYSIS

I. ORGANICS

Caution! Work in vented hood!!!

A. Organic Blank Determination

1. Pour 125 ml of ethyl ether and 125 ml of chloroform into a tared beaker.
2. Evaporate solvent in hood at 70°F or less until no solvent remains.
3. Desiccate the sample in dish for two hours.
4. Weigh the sample to nearest 0.1 mg, record and report on Form LSC-03G.

B. Organic Sample Determination

1. Test for peroxide in sample ether using KI strips. (If KI strip shows positive, contact your supervisor before proceeding.)
2. Transfer the sample solution quantitatively to a 500 ml separatory funnel. Use the first of three 25 ml chloroform aliquots to rinse the sample container.
3. Extract with three 25 ml portions of chloroform. (Shake and vent to release pressure about 4 to 5 times each.) Allow the phases to separate. (Bottom layer is chloroform.) Draw off the bottom layer, transferring the solvent with a funnel containing a plug of sodium sulfate into a tared beaker. (Do not draw off any of the aqueous layer.)
4. After the three chloroform extractions, use two 25 ml portions of chloroform to rinse the sodium sulfate, collecting the rinses in the same tared beaker as the extracts.

5. Next extract the sample three times with 25 ml aliquots of ethyl ether. (Shake and vent to release pressure about 4 to 5 times each.) Allow the phases to separate. (Top layer is ethyl ether.) Draw off the bottom layer (aqueous) into another separatory funnel taking less than 1 ml of the ethyl ether layer with. Decant the ethyl ether, passing it through sodium sulfate and collecting the ethyl ether in the same tared dish as the chloroform.
6. After the three ethyl ether extractions, take two 25 ml portions of ethyl ether and rinse the sodium sulfate collecting the rinses in the same tared beaker as the extracts.
7. Evaporate the solvents (chloroform and ethyl ether) in the tared beaker in the hood at 70°F or less until no solvent remains. (Use no heat and have no sources of ignition in the hood when doing this procedure.) Do not evaporate so quickly as to allow evaporative cooling to lower the temperature of the container below the dew point of water, otherwise, water will be condensed out in the container.
8. Desiccate to constant weight (two hours). Record and report the final weight to the nearest 0.1 mg on Form LSC-03G.

II. INORGANICS

If inorganic residue information is required, the following procedure should be conducted:

A. Inorganic Blank Determination

1. Vent the remaining aqueous phase from the organic extraction in the hood to remove residual organic solvents (usually overnight).
2. Decant the impinger catch into a tared evaporating dish.
3. Evaporate all of the water in the sample in an oven at 100°C. Take care not to boil to prevent bumping and loss of sample.

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4. Cool the dried sample in the desiccator and desiccate until a constant weight is obtained.
5. Report the results to the nearest 0.1 mg on Form LSC-03G.

B. Inorganic Sample Determination

Follow steps 1-5 in Section A above.

NOTES

1. For the organics determination, in the rare event that the impinger catch resulted from a Modified Method 6 determination (SO_2), whereby the solution contains dilute hydrogen peroxide ($\geq 3\%$), do not use ether as an extraction solvent. Substitute toluene for ethyl ether in Section I. (Ether in the presence of peroxide forms explosive hydroperoxide.)
2. In the organics determination, more than three extractions may be required to extract all of the organics. Additional extractions should be performed if the aqueous phase is still cloudy.
3. Special state requirements:
Michigan - Total sample evaporated in tared evaporating dish on steam bath.
Iowa - Organics and inorganics separately, as required.
Wisconsin - Use Method II-8672-WI.
Rest of states - Organics only.

REFERENCES

Proposed standards of Performance for New Stationary Sources, Federal Register 36(159) Part II, August 1, 1979.

Minnesota Pollution Control Agency, Exhibit C.



Flow

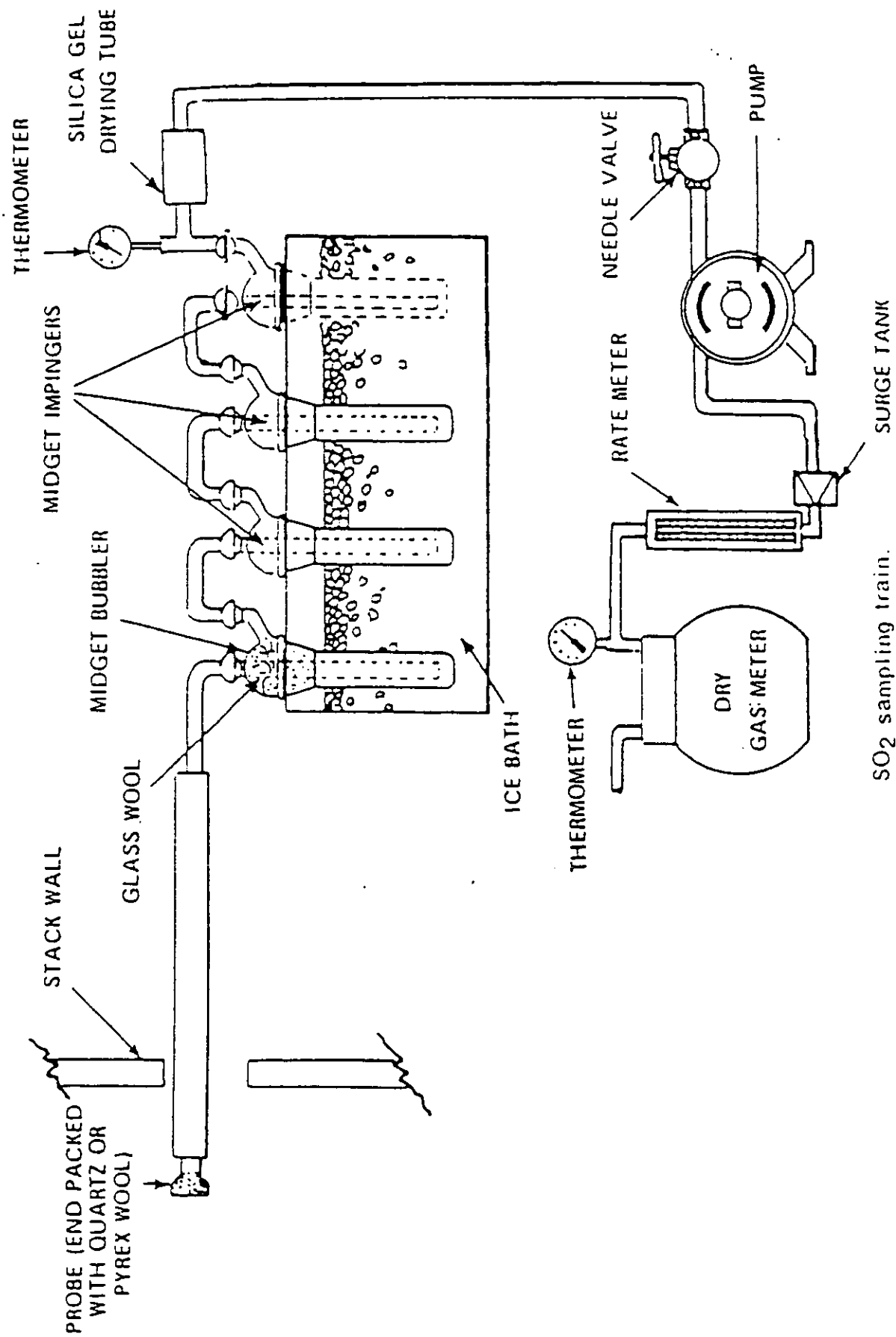
Flow determinations were carried out in accordance with EPA Method 2, CFR Title 40, Part 60, Appendix A (Revised July 1, 1992). A Type S pitot was used to sense velocity pressure and an expanded scale inclined manometer was used to measure pressure. A 24" long bimetallic gauge thermometer was used to measure dry bulb temperatures. Wet bulb temperatures were measured with a mercury thermometer equipped with a cloth wick which was wetted in distilled water immediately prior to taking the reading.

Gas Density and Molecular Weight

Gas compositions were determined as per Method 3 by Orsat analysis of an integrated gas sample collected from the stack during the sulfur dioxide determinations. Standard commercially prepared solutions were used in the Orsat analyzer (sat. KOH carbon dioxide and reduced methylene blue for oxygen).

Sulfur Dioxide Emissions

The sulfur dioxide concentrations were determined per Method 6, CFR Title 40, Part 60, Appendix A (Revised July 1, 1992). In this procedure a gas sample is extracted from the stack with a heated glass-lined probe through a plug of glass wool to remove any flyash. The remaining particulate sulfate, acid mist and sulfur trioxide are separated in an all-glass collection train and the sulfur dioxide fraction collected in a 3% peroxide solution and the resulting sulfate measured by barium-thorin titration method.



SO_2 sampling train.

Flow

Flow determinations were carried out in accordance with EPA Method 2, CFR Title 40, Part 60, Appendix A (Revised July 1, 1987). A type S pitot was used to sense velocity pressure and an inclined manometer was used to measure velocity pressures. Gas temperatures were measured using a calibrated Type K thermocouple and digital temperature meter. Gas density (i.e. molecular weight) was calculated from the composition of the gas which was determined by Orsat.

Gas Flow Density

Gas compositions were determined as per Method 3 by Orsat analysis of an integrated gas sample collected from the stack during the oxides of nitrogen determinations. Standard commercially prepared solutions were used in the Orsat analyzer (sat. KOH for carbon dioxide and reduced methylene blue for oxygen).

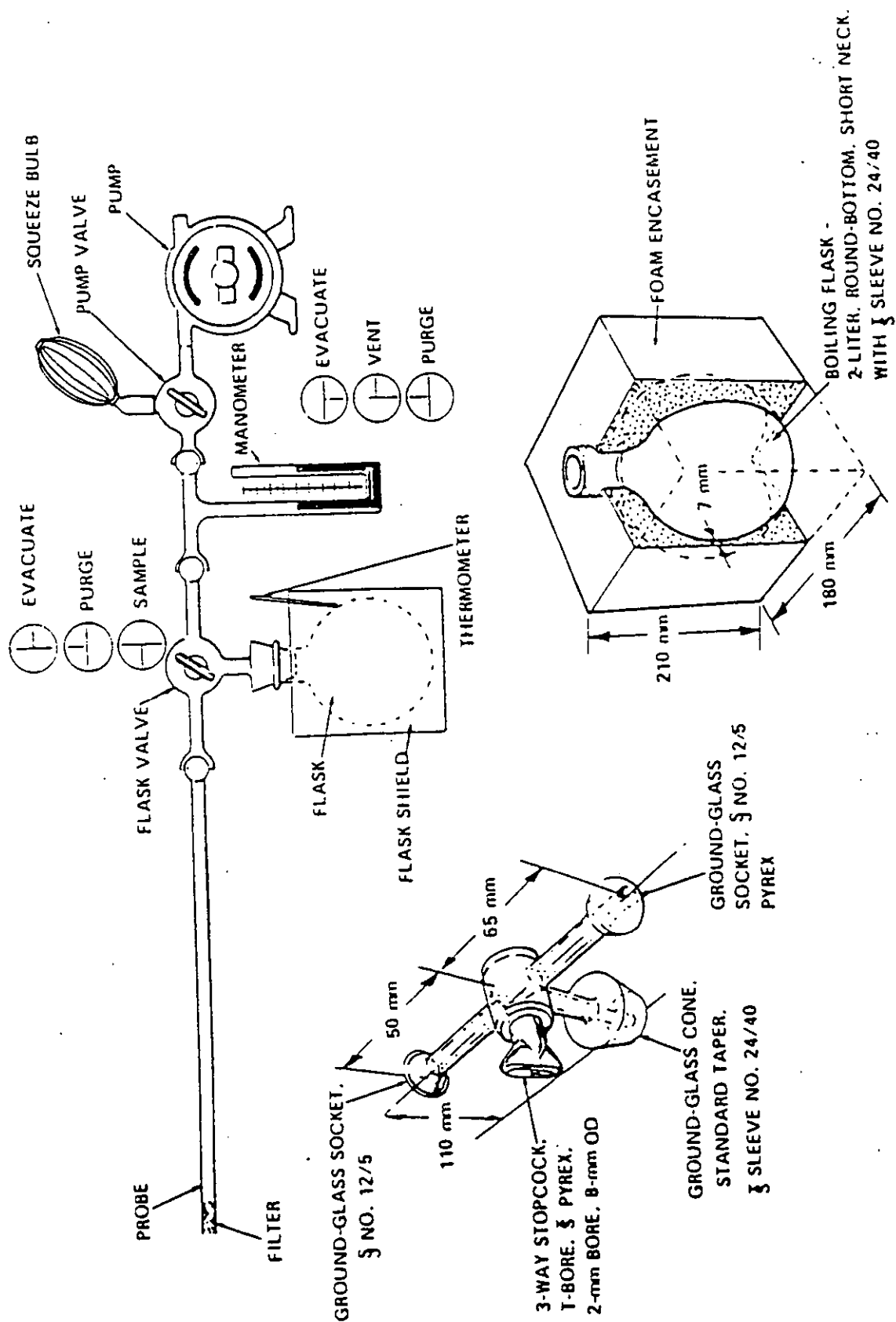
Oxides of Nitrogen

Oxides of nitrogen concentrations were collected in accordance with EPA Method 7 (see above-cited reference) with a specially designed all glass manifold and valving assembly and a heated stainless steel-lined probe. Samples were collected in two-liter evacuated insulated flasks which contained 25 cc of acidified peroxide solution (Method 7 reagent). Nine sets or more of three samples each were collected over a period of 4.5 to 5 hours.

The sampling train was leak checked through the probe at the beginning and end of the test and, in addition, the system leak checked at the time of evacuation of each flask. Before the samples were collected, the probe was purged to eliminate dead volume effects and to raise the temperature of the probe outlet and manifold assembly to minimize condensation of moisture. A plug of microfiber glass wool inserted in the probe inlet was used to prevent particulate material from entering into the flask. The temperature of the flask, vacuum in the

flask and barometric pressure at the time of sampling was recorded for each flask. After sampling was complete, as evidenced by the in-line vacuum gauge, the flask valve was closed, the flask assembly disconnected from the manifold/valve assembly and the flask shook for several minutes to promote oxidation and absorption. The recovered oxides of nitrogen samples were returned to the laboratory and analyzed immediately by ion chromatography as per EPA 7A.

The internal volume of each numbered flask assembly has been measured prior to initial use by filling with water, weighing before and after and then converting the weight of water to volume by means of the density of water at room temperature. Flask volumes are stored in the computer and recalled automatically in the computer calculation.



Sampling train, flask valve, and flask.

APPENDIX H

CALCULATION EQUATIONS

METHOD 2
CALCULATION EQUATIONS

$$\bar{V}_s = 85.49 C_p (\sqrt{\Delta p})_{avg} \sqrt{\frac{T_{s(avg)}}{P_s M_s}}$$

$$Q_{s,d} = 60 (1 - B_{ws}) \bar{V}_s A \left(\frac{528}{T_{s(avg)}} \right) \left(\frac{P_s}{29.92} \right)$$

$$Q_a = 60 \bar{V}_s A$$

$$\dot{m}_g = \frac{4.995 Q_{s,d} G_d}{1 - B_{ws}}$$

$$RH^* = 100 (vp_{wrb} - 0.0003641 P_s (T_{db} - T_{wb})) / vp_{adb}$$

$$B_{ws}^* = RH(vp_{adb}) / P_s$$

$$\rho = \frac{4.585 \times 10^{-2} P_s M_s}{T_s (avg)}$$

*Alternate equations for calculating moisture content from wet bulb and dry bulb data.

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SYMBOLS

A	=	Cross Sectional area of stack, SQ. FT.
A_n	=	Cross sectional area of nozzle, SQ. FT.
B_{ws}	=	Water vapor in gas stream, proportion by volume
C_p	=	Pitot tube coefficient, dimensionless
C_s	=	Concentration of particulate matter in stack gas, wet basis, GR/ACF
C_s	=	Concentration of particulate matter in stack gas, dry basis, corrected to standard conditions, GR/DSCF
EA	=	Excess air, percent by volume
γ	=	Dry test meter correction factor, dimensionless
G_d	=	Specific gravity (relative to air), dimensionless
I	=	Isokinetic variation, percent by volume
M_d	=	Molecular weight of stack gas, dry basis, g/g - mole.
m_s	=	Mass flow of wet flue gas, LB/HR
m_p	=	Particulate mass flow, LB/HR
M_s	=	Molecular weight of stack gas, wet basis, g/g mole.
M_p	=	Total amount of particulate matter collected, g
P_{bar}	=	Atmospheric pressure, IN. HG. (uncompensated)
P_s	=	Stack static gas pressure, IN. WC.
P_s	=	Absolute pressure of stack gas, IN. HG.
P_{std}	=	Standard absolute pressure, 29.92 IN. HG.
A_s	=	Actual volumetric stack gas flow rate, ACFM
$Q_{s, d}$	=	Dry volumetric stack gas flow rate corrected to standard conditions, DSCFM
RH	=	Relative humidity, %

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T_{db}	=	Dry bulb temperature of stack gas. °F
T_{wb}	=	Wet bulb temperature of stack gas. °F
$T_{m(avg)}$	=	Absolute average dry gas meter temperature, °R
$T_{s(avg)}$	=	Absolute average stack temperature. °R
T_{std}	=	Standard absolute temperature. 528 °R (68 °F)
θ	=	Total sampling time, min.
V_{lc}	=	Total volume of liquid collected in impingers and silica gel, ml
V_m	=	Volume of gas sample as measured by dry gas meter, CF
$V_{m(std)}$	=	Volume of gas sample measured by the dry gas meter corrected to standard conditions, DSCF
$V_{w(std)}$	=	Volume of water vapor in the gas sample corrected to standard conditions, SCF
$\bar{V}_1$	=	Average actual stack gas velocity, FT/SEC
vp_{db}	=	Vapor pressure at T_{db} , IN. HG.
vp_{wb}	=	Vapor pressure at T_{wb} , IN. HG.
$\overline{\Delta H}$	=	Average pressure differential across the orifice meter, IN. WC.
ΔP	=	Velocity pressure of stack gas, IN. WC.
γ	=	Dry test meter correction coefficient, dimensionless
ρ	=	Actual gas density, LB/ACF

METHOD 3
CALCULATION EQUATIONS

$$\%EA = \frac{100(\%O_2 - 0.5\% CO)}{0.264\% N_2 - \%O_2 + 0.5\% CO}$$

$$M_d = 0.44(\%CO_2) + 0.32 (\%O_2) + 0.28 (\%N_2 + \%CO)$$

$$M_s = M_d (I - B_{ws}) + 0.18 B_{ws}$$

$$B_{ws} = \frac{V_{w(std)}}{V_{w(std)} + V_{m(std)}}$$

METHOD 5
CALCULATION EQUATIONS

$$V_{m(std)} = 17.65 V_m \gamma \left(\frac{P_{bar} + \overline{\Delta H}/13.6}{T_{m(avg)}} \right)$$

$$V_{w(std)} = 0.0472 V_{Is}$$

$$B_{ws} = \frac{V_{w(std)}}{V_{w(std)} + V_{m(std)}}$$

$$I = 0.0944 \left(\frac{T_{s(avg)} V_{m(std)}}{P_s V_s A_n \theta (I - B_{ws})} \right)$$

$$C_s = \frac{15.43 M_p}{V_{m(std)}}$$

$$C_a = \frac{272.3 M_p P_s}{T_{s(avg)} (V_{w(std)} + V_{m(std)})}$$

$$(\dot{m}_p)_1 = 8.5714 \times 10^{-3} C_s Q_{s,d}$$

$$(\dot{m}_p)_2 = \frac{1.3228 \times 10^{-1} M_p A}{\theta A_n}$$

$$\dot{m}_p = \frac{(\dot{m}_p)_1 + (\dot{m}_p)_2}{2}$$

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CALCULATION EQUATIONS

METHOD 6

$$V_{sd} = 17.64 \frac{V_m P_b \gamma}{T_m} \text{ (MIDGET IMPINGER VERSION)}$$

$$V_{sd} = \frac{17.64 V_m (P_b + \frac{\Delta H}{13.6}) \gamma}{T_m} \text{ (LARGE IMPINGER VERSION)}$$

$$MEQ = (V_i - V_{ib}) N \left(\frac{V_{soln}}{V_a} \right) DF$$

$$C_s = \frac{7.06 \times 10^{-5} MEQ}{V_{sd}}$$

$$E = \frac{20.90 C_s F_d}{20.90 - \bar{B}'_{O_2}} = \frac{F_c C_s}{\bar{B}'_{CO_2}}$$

$$C_s \text{ (MG/DSCM)} = 1.60186 \times 10^7 C_s$$

$$C_s \text{ (GR/DSCF)} = 7000 C_s$$

$$C_s \text{ (ppm, dry)} = 6.02119 \times 10^6 C_s$$

$$C_s \text{ (ppm, wet)} = 6.02119 \times 10^6 C_s \left(1 - \frac{MC}{100} \right)$$

SYMBOLS

$\bar{B}_{O_2}$	=	Average oxygen content in flue gas, % v/v, dry
$\bar{B}_{CO_2}$	=	Average carbon dioxide content in flue gas, % v/v, dry
C_s	=	Concentration of sulfur dioxide in flue gas, dry basis, corrected to standard conditions, LB/DSCF
C_s (GR/DSCF)	=	Concentration of sulfur dioxide in flue gas, dry basis, corrected to standard conditions, GR/DSCF
C_s (MG/DSCM)	=	Concentration of sulfur dioxide in flue gas, dry basis, corrected to standard conditions, MG/DSCM
DF	=	Dilution Factor
E	=	Emission factor, LB of SO_2 /10 ⁶ BTU
F _d	=	Dry oxygen F-Factor for given fuel type, DSCF/10 ⁶ BTU
F _c	=	Carbon dioxide F-Factor for given fuel type, DSCF/10 ⁶ BTU
ΔH	=	Average pressure drop across calibrated orifice, IN. W.C.
Y	=	Dry test meter correction factor, dimensionless
MC	=	Moisture content of flue gas, % v/v
MEQ	=	Total milliequivalents of SO_2 in gas sample
N	=	Normality of barium perchlorate titrant
P _b	=	Barometric pressure at the dry gas meter, IN. HG.
C_s (ppm-dry)	=	Concentration of sulfur dioxide in flue gas, dry basis, (v/v), ppm
C_s (ppm-wet)	=	Concentration of sulfur dioxide in flue gas, wet basis, (v/v), ppm
T _m	=	Absolute average dry gas meter temperature, °R
V _s	=	Volume of sample aliquot titrated, cc
V _m	=	Dry gas volume as measured by the dry gas meter, DCF
V _{std}	=	Dry gas volume as measured by the dry gas meter, corrected to standard conditions (at 68 °F and 1 atmosphere), DSCF

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V_{soln} = Total volume of the solution in which the sulfur dioxide sample is contained, cc

V_t = Volume of barium perchlorate titrant used for the sample, cc (average of replicate titrations)

V_{tb} = Volume of barium perchlorate titrant used for the blank, cc

CALCULATION EQUATIONS

METHOD 7

$$V_{m(std)} = 17.64 (V_f - 25) \left[\frac{P_f}{T_f} - \frac{P_i}{T_i} \right]$$

$$C_s = 6.243 \times 10^{-5} \frac{M}{V_{m(std)}}$$

$$E = \frac{2090 C_s F}{20.9 - \bar{B}_{O_2}}$$

$$C_s (GR/DSCF) = 7000 C_s$$

$$C_s (MG/DSCM) = 1.60186 \times 10^7 C_s$$

$$C_s (ppm-dry) = 8.37552 \times 10^6 C_s$$

$$C_s (ppm-3\% O_2) = 8.37552 \times 10^6 C_s \left\{ 1 + \left[\frac{\bar{B}_{O_2} - 3}{20.9 - \bar{B}_{O_2}} \right] \right\}$$

$$C_s (ppm-wet) = 8.37552 \times 10^6 C_s \left(1 - \frac{MC}{100} \right)$$

SYMBOLS

$\bar{B}_{O_2}$	=	Average oxygen content in flue gas, % v/v
C_s	=	Concentration of nitrogen oxides in flue gas, dry basis, corrected to standard conditions, LB/DSCF
C_s (GR/DSCF)	=	Concentration of nitrogen oxides in flue gas, dry basis, corrected to standard conditions, GR/DSCF
C_s (MG/DSCM)	=	Concentration of nitrogen oxides in flue gas, dry basis, corrected to standard conditions, MG/DSCM
E	=	Emission factor, LB/10 ⁶ BTU
F	=	F-Factor for given fuel type, DSCF/10 ⁶ BTU
M	=	Mass of nitrogen oxides as nitrogen dioxide in gas sample, ug
MC	=	Moisture content of flue gas, %
P_f	=	Final absolute pressure in flask, IN. HG
P_i	=	Initial absolute pressure in flask, IN. HG
C_s (ppm-dry)	=	Concentration of nitrogen oxides in flue gas, dry basis, (v/v), ppm
C_s (ppm-3% O ₂)	=	Concentration of nitrogen oxides in flue gas, dry basis, corrected to 3% O ₂ , (v/v) ppm
C_s (ppm-wet)	=	Concentration of nitrogen oxides in flue gas, wet basis, (v/v), ppm
T_f	=	Final absolute temperature in flask, °R
T_i	=	Initial absolute temperature in flask, °R
V_f	=	Volume of flask and valve, cc
V_{mstdl}	=	Sample volume at standard conditions, dry basis, cc

APPENDIX I

SAMPLING TRAIN CALIBRATION DATA

INTERPOLL LABORATORIES
EPA Method 5 Gas Metering System
Quality Control Check Data Sheet

Job NORTHSHORE MINING

Date 1-9-95

Operator E. T. Tumbler

Module No. 3

Instructions: Operate the control module at a flow rate equal to ΔH_e for 10 minutes before attaching the umbilical. Record the following data:

Bar press 29.58 in. Hg. $T =$ 1.0004 ΔH_e 1.73 in. W.C.

Time (min)	Volume (CF)	Meter Temp. (°F)	
		Inlet	Outlet
	(755.50)		
2.5	757.57	51	40
5.0	759.25	54	40
7.5	761.13	55	41
10	763.00	57	42
	$V_m = 7.50$	Avg(t_m) = <u>49.5</u> °F	

Calculate Y_{on} as follows:

$$Y_{on} = \frac{1.786}{T V_m} \left[\frac{(t_m + 460)}{P_b} \right]^{0.5}$$

$$Y_{on} = \frac{1.786}{(1.0004)(7.50)} \left[\frac{(49.5 + 460)}{(29.58)} \right]^{0.5} = 0.9854$$

$$Y_{on} = \underline{0.9854}$$

If Y_{on} is not within the range of 0.97 to 1.03, "the volume metering system should be investigated before beginning."

CFR Title 40, Part 60, Appendix A, Method 5, Section 4.4.1

S-432

INTERPOLL LABORATORIES
EPA Method 5 Gas Metering System
Quality Control Check Data Sheet

Job Cyprus Northshore Dry Cobble Stone Date 1/12/95
 Operator J.S. Module No. 3

Instructions: Operate the control module at a flow rate equal to $\dot{V}_H$ for 10 minutes before attaching the umbilical. Record the following data:

Bar press 28.94 in. Hg. $\tau =$ 1.004 $\dot{V}_H$ 1.73 in. w.c.

Time (min)	Volume (CF)	Meter Temp. (°F)	
		Inlet	Outlet
	(883.00)		
2.5	884.95	61	59
5.0	886.85	68	61
7.5	888.78	68	61
10	890.77	70	62
	$V_m = 7.77$	Avg(t_m) = 63.8 °F	

Calculate Y_{on} as follows:

$$Y_{on} = \frac{1.786}{\tau V_m} \left[\frac{(t_m + 460)}{P_b} \right]^{0.5}$$

$$Y_{on} = \frac{1.786}{(1.004)(7.77)} \left[\frac{(63.8 + 460)}{(28.94)} \right]^{0.5}$$

$$Y_{on} = \underline{.98}$$

If Y_{on} is not within the range of 0.97 to 1.03, "the volume metering system should be investigated before beginning."

CFR Title 40, Part 60, Appendix A, Method 5, Section 4.4.1

S-432

INTERPOLL LABORATORIES
EPA Method 5 Gas Metering System
Quality Control Check Data Sheet

Job NORTH SHORE

Date 1/10/95

Operator SF

Module No. 15

Instructions: Operate the control module at a flow rate equal to ΔH_e for 10 minutes before attaching the umbilical. Record the following data:

Bar press 29.38 in. Hg. $T =$ 1.0015 ΔH_e 1.85 in. W.C.

Time (min)	Volume (CF)	Meter Temp. (°F)	
		Inlet	Outlet
	(977.40)		
2.5	979.263	66	73
5.0	981.068	68	77
7.5	982.922	66	77
10	984.784	66	79
	$V_m = 7.384$	Avg(t_m) = 71.5 °F	

Calculate Y_{on} as follows:

$$Y_{on} = \frac{1.786}{T V_m} \left[\frac{(t_m + 460)}{P_b} \right]^{0.5}$$

$$Y_{on} = \frac{1.786}{(1.0015)(7.384)} \left[\frac{(71.5 + 460)}{(29.38)} \right]^{0.5}$$

$$Y_{on} = \underline{1.027}$$

If Y_{on} is not within the range of 0.97 to 1.03, "the volume metering system should be investigated before beginning."

CFR Title 40, Part 60, Appendix A, Method 5, Section 4.4.1

S-432

INTERPOLL LABORATORIES
EPA Method 5 Gas Metering System
Quality Control Check Data Sheet

Job CYPRUS SILVER BAY

Date 1-10-95

Operator GH

Module No. 17

Instructions: Operate the control module at a flow rate equal to ΔH for 10 minutes before attaching the umbilical. Record the following data:

Bar press 29.38 in. Hg. $\tau =$.9932 ΔH 1.73 in. W.C.

Time (min)	Volume (CF)	Meter Temp. (°F)	
		Inlet	Outlet
1.0	(85.40)	63	68
2.5	77.225	63	68
5.0	98.703	63	70
7.5	100.932	63	71
10	102.760	63	72
1.0	$V_m = 7.36$	$Avg(t_m) = 66.63^\circ F$	

Calculate Y_{cn} as follows:

$$Y_{cn} = \frac{1.786}{\tau V_m} \left[\frac{(t_m + 460)}{P_b} \right]^{0.5}$$

1.23

$$Y_{cn} = \frac{1.786}{(\cancel{0.9932})(7.36)} \left[\frac{(66.63) + 460}{(29.38)} \right]^{0.5}$$

$$Y_{cn} = \underline{1.034}$$

If Y_{cn} is not within the range of 0.97 to 1.03, "the volume metering system should be investigated before beginning."

CFR Title 40, Part 60, Appendix A, Method 5, Section 4.4.1

S-432

INTERPOL LABORATORIES
EPA Method 5 Gas Metering System
Quality Control Check Data Sheet

Job CYPRUS SILVER BAY

Date 1-11-95

Operator GH

Module No. 17

Instructions: Operate the control module at a flow rate equal to $\dot{V}_H$ for 10 minutes before attaching the umbilical. Record the following data:

Bar press 29.38 in. Hg. $\tau =$.9932 $\dot{V}_H$ 1.73 in. W.C.

Time (min)	Volume (CF)	Meter Temp. (°F)	
		Inlet	Outlet
██████	(<u>95.40</u>)	██████	██████
2.5	97.225	63	68
5.0	98.703	63	70
7.5	100.932	63	71
10	102.760	63	72
██████	$V_m = 7.36$	Avg(t_m) = <u>66.63</u> °F	

Calculate Y_{cn} as follows:

$$Y_{cn} = \frac{1.786}{\tau V_m} \left[\frac{(t_m + 460)}{P_b} \right]^{0.5} \quad 4.23$$

$$Y_{cn} = \frac{1.786}{(\cancel{29.38})(7.36)} \left[\frac{(66.63) + 460}{(29.58)} \right]^{0.5}$$

.9932

$$Y_{cn} = \underline{1.034}$$

If Y_{cn} is not within the range of 0.97 to 1.03, "the volume metering system should be investigated before beginning."

CFR Title 40, Part 60, Appendix A, Method 5, Section 4.4.1

S-432

INTERPOLL LABORATORIES
EPA Method 5 Gas Metering System
Quality Control Check Data Sheet

Job CYPRUS SILVER BAY

Date 1-12-95

Operator GH

Module No. 17

Instructions: Operate the control module at a flow rate equal to $\dot{V}_{He}$ for 10 minutes before attaching the umbilical. Record the following data:

Bar press 29.38 in. Hg. $\tau =$.9932 $\dot{V}_{He}$ 1.73 in. W.C.

Time (min)	Volume (CF)	Meter Temp. (°F)	
		Inlet	Outlet
<u>2.5</u>	<u>97.225</u>	<u>63</u>	<u>68</u>
<u>5.0</u>	<u>98.703</u>	<u>63</u>	<u>70</u>
<u>7.5</u>	<u>100.932</u>	<u>63</u>	<u>71</u>
<u>10</u>	<u>102.760</u>	<u>63</u>	<u>72</u>
	$V_m = 7.36$	Avg(t_m) = <u>66.63</u> °F	

Calculate Y_{on} as follows:

$$Y_{on} = \frac{1.786}{\tau V_m} \left[\frac{(t_m + 460)}{P_b} \right]^{0.5} \quad 4.23$$

$$Y_{on} = \frac{1.786}{(\frac{29.38}{.9932})(7.36)} \left[\frac{(66.63) + 460}{(29.38)} \right]^{0.5}$$

$$Y_{on} = \underline{1.034}$$

If Y_{on} is not within the range of 0.97 to 1.03, "the volume metering system should be investigated before beginning."

CFR Title 40, Part 60, Appendix A, Method 5, Section 4.4.1

S-432

INTERPOLL LABORATORIES
EPA Method 5 Gas Metering System
Quality Control Check Data Sheet

Job CYPRUS N. SHORE

Date 1-13-94

Operator GH

Module No. 17

Instructions: Operate the control module at a flow rate equal to ΔH_e for 10 minutes before attaching the umbilical. Record the following data:

Bar press 29.02 in. Hg. $\tau =$.9932 ΔH_e 1.73 in. W.C.

Time (min)	Volume (CF)	Meter Temp. (°F)	
		Inlet	Outlet
	<u>526.50</u>		
2.5	<u>528.355</u>	<u>60</u>	<u>52</u>
5.0	<u>530.215</u>	<u>60</u>	<u>52</u>
7.5	<u>532.075</u>	<u>61</u>	<u>52</u>
10	<u>533.940</u>	<u>62</u>	<u>52</u>
	$V_m =$ <u>7.44</u>	$Avg(t_m) =$ <u>56.375</u> °F	

Calculate Y_{on} as follows:

$$Y_{on} = \frac{1.786}{\tau V_m} \left[\frac{(t_m + 460)}{P_b} \right]^{0.5}$$

$$Y_{on} = \frac{1.786}{(.9932)(7.44)} \left[\frac{(56.375 + 460)}{(29.02)} \right]^{0.5}$$

$$Y_{on} = \underline{1.02}$$

If Y_{on} is not within the range of 0.97 to 1.03, "the volume metering system should be investigated before beginning."

CFR Title 40, Part 60, Appendix A, Method 5, Section 4.4.1

S-432

INTERPOLL LABORATORIES
EPA Method 5 Gas Metering System
Quality Control Check Data Sheet

Job Northshore W-2 Boiler Stack Date 1/11/95
 Operator J.S. Module No. 18

Instructions: Operate the control module at a flow rate equal to ΔH_e for 10 minutes before attaching the umbilical. Record the following data:

Bar press 29.02 in. Hg. $\tau =$ 1.0026 ΔH_e 1.84 in. W.C.

Time (min)	Volume (CF)	Meter Temp. (°F)	
		Inlet	Outlet
	(115.90)		
2.5	117.69	44	42
5.0	119.55	45	43
7.5	121.43	48	44
10	123.29	50	44
	$V_m = 7.49$	$Avg(t_m) = 45$ °F	

Calculate Y_{on} as follows:

$$Y_{on} = \frac{1.786}{\tau V_m} \left[\frac{(t_m + 460)}{P_b} \right]^{0.5}$$

$$Y_{on} = \frac{1.786}{(1.0026)(7.49)} \left[\frac{(45) + 460}{(29.02)} \right]^{0.5}$$

$$Y_{on} = \underline{.99}$$

If Y_{on} is not within the range of 0.97 to 1.03, "the volume metering system should be investigated before beginning."

CFR Title 40, Part 60, Appendix A, Method 5, Section 4.4.1

S-432

Interpoll Laboratories, Inc.
(612) 786-6020

Meter Box Calibration and Usage Status

Date of Report: January 16, 1995

Meter Box No. : 3 (Rockwell Dry Test Meter Serial No. 949231)

Date of Last Calibration: October 31, 1994

Calibration Technician: E. Trowbridge

Wet Test Meter No.: American Meter AL-20

Date of Use	Report No.	Initial Meter		Final Meter		Volume/Job (cu. ft.)	Total Volume* (cu. ft.)
		Reading		Reading			
November 03, 1994	4-4252	104.00		207.53		103.53	103.53
November 15, 1994	4-4323	225.00		258.73		33.73	137.26
November 29, 1994	4-4436	269.60		480.93		211.33	348.59
December 01, 1994	4-4439	492.60		597.27		104.67	453.26
December 15, 1994	4-4528	598.35		746.40		148.05	601.31
January 10, 1995	5-4664	763.20		1002.16		238.96	840.27

* Total volume through meter since last calibration.

Interpoll Laboratories, Inc.
(612) 786-6020

Meter Box Calibration and Usage Status

Date of Report: January 16, 1995

Meter Box No. : 15 (Rockwell Dry Test Meter Serial No. 1334122)

Date of Last Calibration: October 11, 1994
Calibration Technician: D. Van Hoever
Wet Test Meter No.: American Meter AL-20

Date of Use	Report No.	Initial Meter Reading	Final Meter Reading	Volume/Job (cu. ft.)	Total Volume* (cu. ft.)
November 29, 1994	4-4437	545.60	775.13	229.53	229.53
January 10, 1995	5-4664	813.90	1130.02	316.12	545.65

* Total volume through meter since last calibration.

Interpoll Laboratories, Inc.
(612) 786-6020

Meter Box Calibration and Usage Status

Date of Report: January 16, 1995

Meter Box No. : 17 (Rockwell Dry Test Meter Serial No. 1334113)

Date of Last Calibration: October 31, 1994

Calibration Technician: E. Trowbridge

Wet Test Meter No.: American Meter AL-20

Date of Use	Report No.	Initial Meter Reading	Final Meter Reading	Volume/Job (cu. ft.)	Total Volume* (cu. ft.)
January 10, 1995	5-4664	932.80	1525.47	592.67	592.67

* Total volume through meter since last calibration.

Interpoll Laboratories, Inc.
(612) 786-6020

Meter Box Calibration and Usage Status

Date of Report: January 16, 1995

Meter Box No. : 18 (Rockwell Dry Test Meter Serial No. 1334117)

Date of Last Calibration: October 31, 1994
Calibration Technician: E. Trowbridge
Wet Test Meter No.: American Meter AL-20

Date of Use	Report No.	Initial Meter		Final Meter		Volume/Job (cu. ft.)	Total Volume* (cu. ft.)
		Reading		Reading			
December 06, 1994	4-4505	666.33		897.50		231.17	231.17
December 12, 1994	4-4524	915.40		1115.15		199.75	430.92
January 12, 1995	5-4664	1123.70		1299.88		176.18	607.10

* Total volume through meter since last calibration.

Meter Calibration Sheet EPA/Method 5

Control Module No.
Serial No. DTM
Technician

☐ readjusted linkage
☐ changed dry test meter

Meter was not in tolerance
 Meter was not in tolerance
 Date 11/11/94

Positive leak check performed by
Meter was in tolerance
Approved by

*Based on Al-20 wet test meter calibration in Nov. 1991 against Bell Prover (NBS Traceable) - Carl Poe Co.

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(612) 786-6020

Date 10/11/94 Control Module No. 15
Bar. Press. 29.24 IN.HG 1334122
Wet Test Meter No. AL-20 Technician D. Van Hoever

[illegible]

Positive leak check performed by

Meter was in tolerance.

Approved by

Meter was not in tolerance

Meter was not in tolerance

Date _____

□: readjusted linkage

☐: changed dry test meter

10/12/94

*Based on AL-20 wet test meter calibration in November 1991 against Bell Prover (NBS Traceable) - Carl Poe Co.

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(612) 786-6020

Meter Calibration Sheet EPA/Method 5

Date _____

Bar. Press.

Wel Test Meter No.

75-15-01

29,11 IN:HG

AL-20

Control Module No.

Serial No. DTM

Technician

ΔH (IN.WC)		Gas Volume Wet Test Meter (ft ³)	Cal. Index ϕ	Diff. Wet Test Meter ΔP_w (IN.WC.)	Gas Volume Dry Test Meter (ft ³)		Gas Temperatures				Time θ	Meter Coeff.	Orifice Const.	C _i	
					Nominal	Actual	V _w	V _d	Wet Test T _w (°F)	Dry Test					
										T _a (°F)					T _b (°F)
0.5	1.5	2	99.85	0.01	916.000	918.048	67.5	51	72	4/48	.9904	1.63			
1.2	1.2	3	99.91	0.025	912.500	915.610	67.5	80	71	4/47	.9912	1.73			
2.0	2.0	3	99.93	0.055	918.500	921.566	67.5	87	73	3/46	.9957	1.77			
3.3	3.3	5	100.00	0.09	922.000	927.122	67.0	90	74	3/52	.9954	1.74			
4.7	4.7	5	100.02	0.12	927.500	932.627	67.0	92	75	4/08	.9934	1.79			

Positive leak check performed by
Meter was in tolerance
Approved by

Meter was not in tolerance

Meter was not in tolerance,

Dale

☐: readjusted linkage
☐: changed dry test meter

tolerance 11/1/94

Approved by _____
 Approved by _____
 *Based on A-20 wet test meter calibration in Nov, 1991 against Bell Prover (NBS Traceable) - Carl Poe Co.

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Meter Calibration Sheet EPA/Method 5

Control Module No.
Serial No. DTM
Technician

18
1334117
E. Trowbridge

Positive leak check performed by _____
 Meter was in tolerance ☒ Meter was not in tolerance ☐
 Approved by [Signature] Date 4/11/94
 *Based on AL-20 wet test meter calibration in Nov. 1991 against Bell Prover (NBS Traceable) - Carl Poe Co.

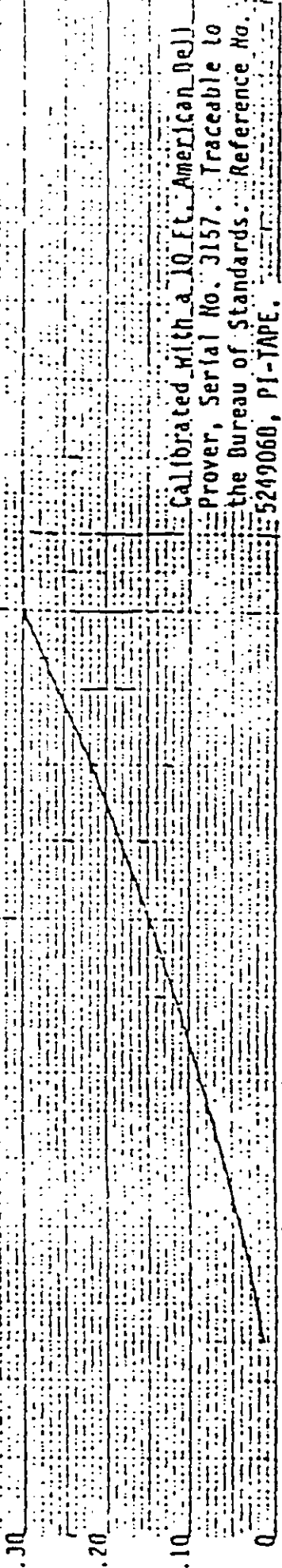
☐: readjusted linkage
☐: changed dry test meter

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WET TEST METER

PULSATION RANGE

DIFFERENTIAL - INCHES H2O



Calibrated with a 10 Ft. American Bell Prover, Serial No. 3157. Traceable to the Bureau of Standards. Reference No. 5249060, PI-TAPE.

AL-20 American Wet Test Meter Serial No. 717

Stainless Steel w/Removable Back

Calibrated w/Saturated Air

Water Temp. 74° F.

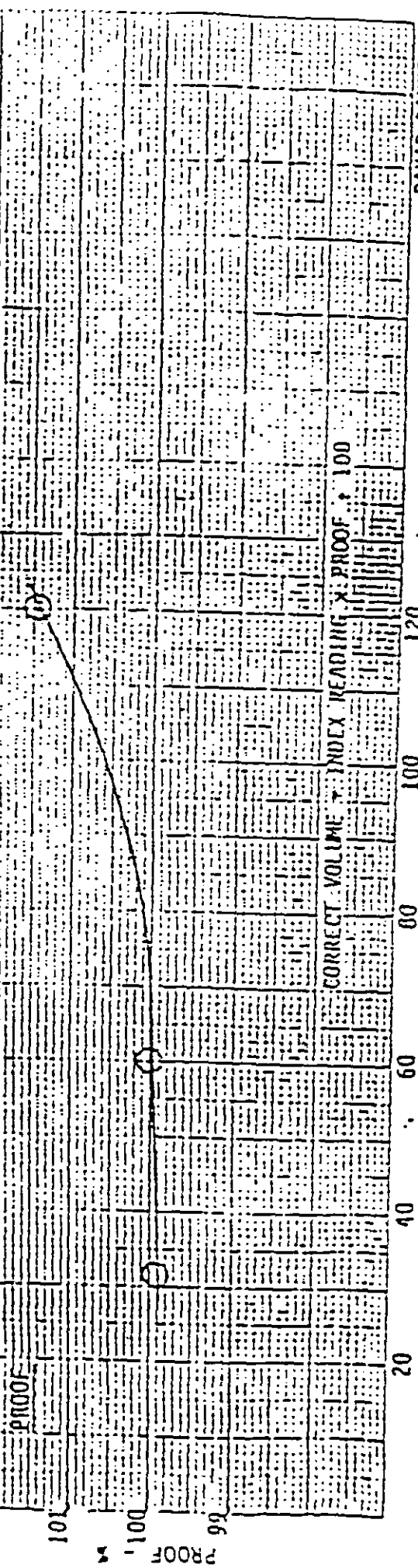
Air Temp. 74° F.

Inlet Pressure 2" H2O Constant

Calibration Rate: 60 CFH Per/Hr.

Capacity Rate: 120 CFH Per/Hr.

Restricted Outlet for Rate Deviation



DAVID DANKS

FLOW RATE - CUBIC FEET OF AIR PER HOUR

Interpoll Laboratories, Inc.
(612) 786-6020

Nozzle Calibration
Data Sheet

Date of Calibration: 01-10-95

Nozzle Number 3-3

Technician: Ed Trowbridge

The nozzle is rotated in 60 degree increments and the diameter at each point is measured to the nearest 0.001 inch. The observed readings and average are shown below.

Position	Diameter (inches)
1	.185
2	.187
3	.186
Average:	.186

Interpoll Laboratories, Inc.
(612) 786-6020

Nozzle Calibration
Data Sheet

Date of Calibration: 01-10-95

Nozzle Number 7-4

Technician: Duane Van Hoever

The nozzle is rotated in 60 degree increments and the diameter at each point is measured to the nearest 0.001 inch. The observed readings and average are shown below.

Position	Diameter (inches)
1	.247
2	.247
3	.246
Average:	.247

Interpoll Laboratories, Inc.
(612) 786-6020

Nozzle Calibration
Data Sheet

Date of Calibration: 01-10-95

Nozzle Number 1-4

Technician: Gary Hove

The nozzle is rotated in 60 degree increments and the diameter at each point is measured to the nearest 0.001 inch. The observed readings and average are shown below.

Position	Diameter (inches)
1	.249
2	.251
3	.250
Average:	.250

Interpoll Laboratories, Inc.
(612) 786-6020

Nozzle Calibration
Data Sheet

Date of Calibration: 01-12-95
Technician: Gary Hove

Nozzle Number 1-3

The nozzle is rotated in 60 degree increments and the diameter at each point is measured to the nearest 0.001 inch. The observed readings and average are shown below.

Position	Diameter (inches)
1	.185
2	.184
3	.185
Average:	.185

Interpoll Laboratories, Inc.
(612) 786-6020

Nozzle Calibration
Data Sheet

Date of Calibration: 01-13-95
Technician: Gary Hove

Nozzle Number 1-4

The nozzle is rotated in 60 degree increments and the diameter at each point is measured to the nearest 0.001 inch. The observed readings and average are shown below.

Position	Diameter (inches)
1	.250
2	.250
3	.249
Average:	.250

Interpoll Laboratories, Inc.
(612) 786-6020

Nozzle Calibration
Data Sheet

Date of Calibration: 01-13-95

Nozzle Number 3-3

Technician: Jeff Scriptor

The nozzle is rotated in 60 degree increments and the diameter at each point is measured to the nearest 0.001 inch. The observed readings and average are shown below.

Position	Diameter (inches)
1	.182
2	.182
3	.181
Average:	.182

Interpoll Laboratories, Inc.

Temperature Measurement Device
Calibration Sheet

Unit under test:

Vendor BECKMAN INDUSTRIAL
Model HD 110 T Serial Number PDT #18
Range 0 - 2000 °F Thermocouple Type K
Date of Calibration 11/2/94 Technician D. VAN HOEVER

Method of Calibration:

- ☐ Comparison against ASTM mercury in glass thermometer using a thermostatted and insulated aluminum block designed to provide uniform temperature. The temperature is adjusted by adjusting the voltage on the block heater cartridge.
- ☒ Omega Model CL-300 Type K Thermocouple Simulator which provides 22 precise temperature equivalent millivolt signals. The CL-300 is cold junction compensated. Calibration accuracy is $\pm 0.1\%$ of span (2100°F) ± 1 degree (for negative temperatures add ± 2 degrees. The CL-300 simulates exactly the millivoltage of a Type K thermocouple at the indicated temperature.

Desired Temp (°F) Nominal	Temperature of Standard or Simulated Temp (°F)	Response of Unit Under Test (°F)	Deviation	
			Δt (°F)	(%)
0		-2	-2	.43
100		94	6	1.07
200		198	2	.50
300		296	4	.53
400		393	7	.81
500		493	7	.73
600		596	4	.38
700		696	4	.34
800		802	2	.16
900		802 904	4	.29
1000		1009	9	.58
1100		1113	13	.83
1200		1219	19	1.14
1300		1320	20	1.14
1400		1424	24	1.27
1500		1522	22	1.13
1600		1624	24	1.17
1700		1719	19	.88
1800		1818	18	.80
1900		1910	10	.42
2000		—	—	—
2100		—	—	—
		Averages:		.72

OF = off scale response by unit under test (°F)
% dev = $100 \Delta t / (460 + t)$

- ☒ Unit in tolerance
☐ Unit was not in tolerance: recalibrated - See new calibration sheet.

Interpoll Laboratories, Inc.

Temperature Measurement Device
Calibration Sheet

NO 25

Unit under test:

Vendor BECKMAN
Model HO 110 T Serial Number 25
Range _____ °F Thermocouple Type K
Date of Calibration 10-28-94 Technician GH

Method of Calibration:

- ☐ Comparison against ASTM mercury in glass thermometer using a thermostatted and insulated aluminum block designed to provide uniform temperature. The temperature is adjusted by adjusting the voltage on the block heater cartridge.
- ☐ Omega Model CL-300 Type K Thermocouple Simulator which provides 22 precise temperature equivalent millivolt signals. The CL-300 is cold junction compensated. Calibration accuracy is $\pm 0.1\%$ of span (2100°F) ± 1 degree (for negative temperatures add ± 2 degrees. The CL-300 simulates exactly the millivoltage of a Type K thermocouple at the indicated temperature.

Desired Temp (°F) Nominal	Temperature of Standard or Simulated Temp (°F)	Response of Unit Under Test (°F)	Deviation	
			Δt (°F)	(%)
0	0	0	0	0
100	100	91	9	1.61
200	200	194	6	0.99
300	300	291	9	1.84
400	400	390	10	1.16
500	500	489	11	1.04
600	600	592	8	0.75
700	700	692	8	0.68
800	800	798	2	0.15
900	900	900	0	0
1000	1000	1005	5	0.34
1100	1100	1108	8	0.44
1200	1200	1191	9	0.58
1300	1300	1315	15	0.95
1400	1400	1397	3	0.17
1500	1500	1498	2	0.10
1600	1600	1602	2	0.09
1700	1700	1697	3	0.20
1800	1800	1796	4	0.22
1900	1900	1889	11	0.46
2000	2000	1984	16	0.65
2100				
		Averages:	7/4	1.0096

OF = off scale response by unit under test (°F)
% dev = $100 \Delta t / (460 + t)$

- ☐ Unit in tolerance.
☐ Unit was not in tolerance: recalibrated - See new calibration sheet.

Interpoll Laboratories, Inc.

Temperature Measurement Device
Calibration Sheet

Unit under test:

Vendor Omega # 34
Model HH 81 Serial Number 74TX 0343
Range 0-2000 °F Thermocouple Type K
Date of Calibration 1-11-95 Technician E. TROUBIDOP

Method of Calibration:

- ☐ Comparison against ASTM mercury in glass thermometer using a thermostatted and insulated aluminum block designed to provide uniform temperature. The temperature is adjusted by adjusting the voltage on the block heater cartridge.
- ☒ Omega Model CL-300 Type K Thermocouple Simulator which provides 22 precise temperature equivalent millivolt signals. The CL-300 is cold junction compensated. Calibration accuracy is $\pm 0.1\%$ of span (2100 °F) ± 1 degree (for negative temperatures add ± 2 degrees. The CL-300 simulates exactly the millivoltage of a Type K thermocouple at the indicated temperature.

Desired Temp (°F) Nominal	Temperature of Standard or Simulated Temp (°F)	Response of Unit Under Test (°F)	Deviation	
			Δt (°F)	(%)
0	0	-3	-3	.65
100	100	98	2	.35
200	200	201	1	.16
300	300	299	1	.13
400	400	398	2	.23
500	500	499	1	.10
600	600	600	0	0
700	700	699	1	.08
800	800	802	2	.15
900	900	901	1	.07
1000	1000	1001	1	.06
1100	1100	1100	0	0
1200	1200	1202	2	.01
1300	1300	1301	1	.05
1400	1400	1403	3	.16
1500	1500	1501	1	.05
1600	1600	1604	4	.19
1700	1700	1703	3	.13
1800	1800	1804	4	.17
1900	1900	1902	2	.05
2000	2000	2003	3	.12
2100	2100	2100	0	0
		Averages:	1.77	.227

OF = off scale response by unit under test (°F)
% dev = $100 \Delta t / (460 + t)$

- ☒ Unit in tolerance
☐ Unit was not in tolerance; recalibrated - See new calibration sheet.

Interpoll Laboratories, Inc.

Temperature Measurement Device
Calibration Sheet

Unit under test:

Vendor OMEGA
Model 144 81 Serial Number PDT # 35
Range _____ °F Thermocouple Type K
Date of Calibration 11/2/94 Technician D. Van Hever

Method of Calibration:

- ☐ Comparison against ASTM mercury in glass thermometer using a thermostatted and insulated aluminum block designed to provide uniform temperature. The temperature is adjusted by adjusting the voltage on the block heater cartridge.
- ☒ Omega Model CL-300 Type K Thermocouple Simulator which provides 22 precise temperature equivalent millivolt signals. The CL-300 is cold junction compensated. Calibration accuracy is $\pm 0.1\%$ of span (2100°F) ± 1 degree (for negative temperatures add ± 2 degrees. The CL-300 simulates exactly the millivoltage of a Type K thermocouple at the indicated temperature.

Desired Temp (°F) Nominal	Temperature of Standard or Simulated Temp (°F)	Response of Unit Under Test (°F)	Deviation	
			Δt (°F)	(%)
0		-6	6	1.3
100		95	5	.89
200		197	3	.15
300		295	5	.66
400		395	5	.58
500		496	4	.42
600		598	2	.19
700		697	3	.26
800		800	—	0
900		898	2	.15
1000		999	1	.07
1100		1098	2	.13
1200		1199	1	.06
1300		1298	2	.11
1400		1400	—	0
1500		1500	—	0
1600		1602	2	.10
1700		1701	1	.05
1800		1802	2	.09
1900		1901	1	.04
2000		2001	1	.04
2100		2099	1	.04
		Averages:		.26

OF = off scale response by unit under test (°F)
% dev = $100 \Delta t / (460 + t)$

- ☒ Unit in tolerance
☐ Unit was not in tolerance: recalibrated - See new calibration sheet.

Interpoll Laboratories, Inc.

Temperature Measurement Device
Calibration Sheet

Unit under test:

Vendor OMEGA
Model HH81 Serial Number 74JX1119
Range -160 - 1372°C °R Thermocouple Type K
Date of Calibration 10/10/94 Technician EJ

40

Method of Calibration:

- ☐ Comparison against ASTM mercury in glass thermometer using a thermostatted and insulated aluminum block designed to provide uniform temperature. The temperature is adjusted by adjusting the voltage on the block heater cartridge.
- ☒ Omega Model CL-300 Type K Thermocouple Simulator which provides 22 precise temperature equivalent millivolt signals. The CL-300 is cold junction compensated. Calibration accuracy is $\pm 0.1\%$ of span (2100°F) ± 1 degree (for negative temperatures add ± 2 degrees. The CL-300 simulates exactly the millivoltage of a Type K thermocouple at the indicated temperature.

Desired Temp ($^{\circ}\text{F}$) Nominal	Temperature of Standard or Simulated Temp ($^{\circ}\text{F}$)	Response of Unit Under Test ($^{\circ}\text{F}$)	Deviation	
			Δt ($^{\circ}\text{F}$)	(%)
0	0	-3.0	3	.65
100	100	98	2	.36
200	200	200	0	0
300	300	292	2	.26
400	400	393	2	.23
500	500	499	1	.10
600	600	600	0	0
700	700	699	1	.03
800	800	801	1	.03
900	900	900	0	0
1000	1000	1001	1	.07
1100	1100	1099	1	.06
1200	1200	1201	1	.06
1300	1300	1299	1	.06
1400	1400	1402	2	.11
1500	1500	1500	0	0
1600	1600	1602	2	.09
1700	1700	1700	0	0
1800	1800	1802	2	.09
1900	1900	1901	1	.04
2000	2000	2001	1	.04
2100	2100	2099	1	.04
		Averages:	1.1	.11

OF = off scale response by unit under test ($^{\circ}\text{F}$)
% dev = $100 \Delta t / (460 + t)$

- ☒ Unit in tolerance
☐ Unit was not in tolerance: recalibrated - See new calibration sheet.

INTERPOLL LABORATORIES
(612)786-6020
Stack Sampling Department - QA
Aneroid Barometer Calibration Sheet

Date 7-20-94
Technician GH
Mercury Column Barometer No. NO 1
Aneroid Barometer No. GARY HIVE 1036235

Actual Mercury Barometer Read	Ambient Temp.	Temperature Correction Factor	Adjusted Mercury Barometer Read	Initial Aneroid Barometer Read	Difference (P _{ba} -P _{bm})
29.05	75	-.124	28.925	28.940	-.015

Has this barometer shown any consistent problems with calibration? Yes/No. If yes, explain. YES ADD ADJUSTED IT

Has problem been alleviated? Yes/No. How? YES

***Note**

Aneroid barometers will be calibrated periodically against a mercury column barometer. The aneroid barometer to be calibrated should be placed in close proximity to the mercury barometer and left to equilibrate for 20-30 minutes before calibrating. Aneroid barometer will be calibrated to the adjusted mercury barometer readings.

S-312

INTERPOLL LABORATORIES
(612)786-6020

ET'S

Stack Sampling Department - QA
Aneroid Barometer Calibration Sheet

Date 1-11-95
Technician E. Thowick
Mercury Column Barometer No. ULTIMETER MODEL 12
Aneroid Barometer No. SN - P1002005

Actual Mercury Barometer Read	Ambient Temp.	Temperature Correction Factor	Adjusted Mercury Barometer Read	Initial Aneroid Barometer Read	Difference (Pba-Pbm)
28.86	72	.113	28.747	28.68	.067

Has this barometer shown any consistent problems with calibration? Yes/No. No If yes, explain. _____

Has problem been alleviated? Yes/No. How? _____

*Note

Aneroid barometers will be calibrated periodically against a mercury column barometer. The aneroid barometer to be calibrated should be placed in close proximity to the mercury barometer and left to equilibrate for 20-30 minutes before calibrating. Aneroid barometer will be calibrated to the adjusted mercury barometer readings.

S-312

INTERPOLL LABORATORIES
(612)786-6020
Stack Sampling Department - QA
Aneroid Barometer Calibration Sheet

Date 11/2/94
Technician D. VanHoever
Mercury Column Barometer No. LAB
Aneroid Barometer No. 2011

Actual Mercury Barometer Read	Ambient Temp.	Temperature Correction Factor	Adjusted Mercury Barometer Read	Initial Aneroid Barometer Read	Difference (Pba-Pbm)
28.81	76	.134	28.67	28.66	.01

Has this barometer shown any consistent problems with calibration? Yes No. If
yes, explain. _____

Has problem been alleviated? Yes/No. How? _____

*Note

Aneroid barometers will be calibrated periodically against a mercury column barometer. The aneroid barometer to be calibrated should be placed in close proximity to the mercury barometer and left to equilibrate for 20-30 minutes before calibrating. Aneroid barometer will be calibrated to the adjusted mercury barometer readings.

S-312

S-Type Pitot Tube Inspection Sheet

Pitot Tube No. 23-5

Pitot tube dimensions:

1. External tubing diameter (D) 3.16 IN.
2. Base to Side A opening plane (P_A) 4.60 IN.
3. Base to Side B opening plane (P_B) 4.60 IN.

Alignment:

4. α_1 < 10° 0
5. α_2 < 10° 0

6. β_1 < 5° 0
7. β_2 < 5° 0

8. Z < .125" .02
9. W < .0625" .01

Distance from Pitot to Probe Components:

10. Pitot to 0.500 IN. nozzle 7.60 IN.
11. Pitot to probe sheath 3.0 IN.
12. Pitot to thermocouple (parallel to probe) 3.0 IN.
13. Pitot to thermocouple (perpendicular to probe) 7.60 IN.

- ☒ Meets all EPA design criteria thus $C_p = 0.84$
☐ Does not meet EPA design criteria - thus calibrate in wind tunnel.
 $C_p =$ _____

Date of Inspection:

2/8-94

Inspected by:

[Signature]

S-Type Pitot Tube Inspection Sheet

Pitot Tube No. 23-6

Pitot tube dimensions:

1. External tubing diameter (D) .316 IN.
2. Base to Side A opening plane (P_A) .460 IN.
3. Base to Side B opening plane (P_B) .460 IN.

Alignment:

4. α_1 < 10° 0
5. α_2 < 10° 0
6. β_1 < 5° 0
7. β_2 < 5° 0
8. Z < .125" .02
9. W < .0625" .025

Distance from Pitot to Probe Components:

10. Pitot to 0.500 IN. nozzle .750 IN.
11. Pitot to probe sheath 3.0 IN.
12. Pitot to thermocouple (parallel to probe) 3.0 IN.
13. Pitot to thermocouple (perpendicular to probe) .760 IN.

- ☒ Meets all EPA design criteria thus $C_p = 0.84$
☐ Does not meet EPA design criteria - thus calibrate in wind tunnel.
 $C_p =$ _____

Date of Inspection:

4-8-94

Inspected by:

[Signature]

S-Type Pitot Tube Inspection Sheet

Pitot Tube No. 23-10

Pitot tube dimensions:

1. External tubing diameter (D_t) 1.316 IN.
2. Base to Side A opening plane (P_A) 1.460 IN.
3. Base to Side B opening plane (P_B) 1.460 IN.

Alignment:

4. α_1 < 10° 0
5. α_2 < 10° 0

6. β_1 < 5° 0
7. β_2 < 5° 0

8. Z < .125" .02
9. W < .0625" .025

Distance from Pitot to Probe Components:

10. Pitot to 0.500 IN. nozzle 1.750 IN.
11. Pitot to probe sheath 3.0 IN.
12. Pitot to thermocouple (parallel to probe) 3.0 IN.
13. Pitot to thermocouple (perpendicular to probe) 1.760 IN.

- ☒ Meets all EPA design criteria thus $C_p = 0.84$
☐ Does not meet EPA design criteria - thus calibrate in wind tunnel.
 $C_p =$ _____

Date of Inspection:

4-8-94

Inspected by:

[Signature]

S-Type Pitot Tube Inspection Sheet

Pitot Tube No. 24-2 1/2

Pitot tube dimensions:

1. External tubing diameter (D_t) .316 IN.
2. Base to Side A opening plane (P_A) .460 IN.
3. Base to Side B opening plane (P_B) .460 IN.

Alignment:

4. α_1 $< 10^\circ$ 0
5. α_2 $< 10^\circ$ 0
6. B_1 $< 5^\circ$ 0
7. B_2 $< 5^\circ$ 0
8. Z $< .125"$.0
9. W $< .0625"$.02

Distance from Pitot to Probe Components:

10. Pitot to 0.500 IN. nozzle .750 IN.
11. Pitot to probe sheath 3.0 IN.
12. Pitot to thermocouple (parallel to probe) 3.0 IN.
13. Pitot to thermocouple (perpendicular to probe) .760 IN.

- ☒ Meets all EPA design criteria thus $C_p = 0.84$
☐ Does not meet EPA design criteria - thus calibrate in wind tunnel.
 $C_p =$ _____

Date of Inspection:

4-8-94

Inspected by:

[Signature]

S-Type Pitot Tube Inspection Sheet

Pitot Tube No. 24-4

Pitot tube dimensions:

1. External tubing diameter (D_t) .316 IN.
2. Base to Side A opening plane (P_A) .460 IN.
3. Base to Side B opening plane (P_B) .460 IN.

Alignment:

4. α_1 < 10° 0
5. α_2 < 10° 0
6. B_1 < 5° 0
7. B_2 < 5° 0
8. Z < .125" .02
9. W < .0625" .01

Distance from Pitot to Probe Components:

10. Pitot to 0.500 IN. nozzle .750 IN.
11. Pitot to probe sheath 3.0 IN.
12. Pitot to thermocouple (parallel to probe) 3.0 IN.
13. Pitot to thermocouple (perpendicular to probe) .760 IN.

- ☒ Meets all EPA design criteria thus $C_p = 0.84$
☐ Does not meet EPA design criteria - thus calibrate in wind tunnel.
 $C_p =$ _____

Date of Inspection:

11-8-84

Inspected by:

[Signature]

Interpoll Laboratories, Inc.
(612) 786-6020

S-Type Pitot Tube Inspection Sheet

Pitot Tube No. 24-6

Pitot tube dimensions:

1. External tubing diameter (D_t) 3.16 IN.
2. Base to Side A opening plane (P_A) 4.60 IN.
3. Base to Side B opening plane (P_B) 4.60 IN.

Alignment:

4. α_1 < 10° 0
5. α_2 < 10° 0
6. B_1 < 5° 0
7. B_2 < 5° 0
8. Z < .125" .02
9. W < .0625" 0

Distance from Pitot to Probe Components:

10. Pitot to 0.500 IN. nozzle 7.50 IN.
11. Pitot to probe sheath 3.0 IN.
12. Pitot to thermocouple (parallel to probe) 3.0 IN.
13. Pitot to thermocouple (perpendicular to probe) 7.50 IN.

- ☒ Meets all EPA design criteria thus $C_p = 0.84$
☐ Does not meet EPA design criteria - thus calibrate in wind tunnel.
 $C_p =$ _____

Date of Inspection:

4-8-84

Inspected by:

G. T. [Signature]

S-Type Pitot Tube Inspection Sheet

Pitot Tube No. 29-4

Pitot tube dimensions:

1. External tubing diameter (D_t) 1.316 IN.
2. Base to Side A opening plane (P_A) 4.60 IN.
3. Base to Side B opening plane (P_B) 4.60 IN.

Alignment:

4. α_1 $< 10^\circ$ 0
5. α_2 $< 10^\circ$ 0

6. B_1 $< 5^\circ$ 0
7. B_2 $< 5^\circ$ 0

8. Z $< .125"$.02
9. W $< .0625"$.02

Distance from Pitot to Probe Components:

10. Pitot to 0.500 IN. nozzle 1.750 IN.
11. Pitot to probe sheath 3.0 IN.
12. Pitot to thermocouple (parallel to probe) 3.0 IN.
13. Pitot to thermocouple (perpendicular to probe) 1.760 IN.

- ☒ Meets all EPA design criteria thus $C_p = 0.84$
☐ Does not meet EPA design criteria - thus calibrate in wind tunnel.
 $C_p =$ _____

Date of Inspection:

4-7-94

Inspected by:

[Signature]

APPENDIX J

TEST PLAN

CYPRUS NORTSHORE MINING
E.W. Davis Works
Compliance and Re-test Plan

PART I. GENERAL INFORMATION

Test Plan Date:	December 3, 1994
Test Date:	Week of January 9, 1995
Name & Address of Emission Facility:	Northshore Mining Company 10 Outer Drive Silver Bay, MN 55614
Permittee Contact:	Dennis M. Wagner (218/226-6056)
Permit File No.:	27A-89-OT-1
Independent Testing Company:	Interpoll Laboratories
Contact Person:	Kathy Eickstadt (612/786-7854)
Sources to be tested:	
Emission source 11:	Fine Crusher bag house.
Emission source 76:	Pelletizing furnace discharge rotoclone.
Emission source 104-105:	Pelletizer furnace 11 waste gas WWESP.
Emission source 106-107:	Pelletizer furnace 12 waste gas WWESP.
Reason for testing:	Compliance tests and compliance test re-test.
Physical descriptions of emission points: Drawings of emission control points are attached for Agency review.	

PART II TESTING REQUIREMENTS

Emission Source	Pollutant	Emission Limit	Applicable MN Rule	Methods	Run Length
11 Fine Crusher	Particulate Matter	0.002 Gr/DSCFM	7005.0010- 7005.0080	5	60 Min
76 Pelletizer Rotoclone	Particulate Matter	0.03 Gr/DSCFM	7005.0010- 7005.0080	5	60 Min
	Opacity	20%	7005.0470 Subp. 1.B.	9	60 Min
104, 105 & 106 Pelletizer Waste Gas	Particulate Matter	0.01 Gr/DSCFM	7005.0010- 7005.0080	5	60 Min
	Amphiboles Fibers (1)		—	MDH	1-60 Min
107 Pelletizer Waste Gas	Particulate Matter	0.01 Gr/DSCFM	7005.0010- 7005.0080	5	60 Min
	SO ₂	—	—	6C	60 Min
	NO _x	—	—	7E	60 Min

PART III OPERATING CONDITIONS

Emission Source 11:

Process Equipment:	Crude ore crushing.
Process Operating Rate During Test:	Normal 400-600 TPH.
Control Equipment:	Bag house.
Control Equipment Operating Parameters:	Pressure drop.
Rationale for Worst Case:	None
Normal Operating Range:	15,000 ACEM @ 77° F rated.
Air Pollution Control and Process Monitoring:	Tons crushed during test period will be recorded.

Emission Source 76:

Process Equipment:	Pelletizer furnace discharge rotoclone.
Process Operating Rate During Test Period:	Normal 230-250 TPH.
Control Equipment:	Rotoclone.
Control Equipment Operating Parameters:	None.
Rationale for Worst Case:	None.
Normal Operating Range:	32,000 ACFM @ 750° F.
Air Pollution Control & Process Monitoring:	Tons processed during test period will be recorded.

Emission Sources 104-107:

Process Equipment:	Pelletizing furnace waste gas.
Process Operating Rate During Test:	Normal 230-250 TPH.
Control Equipment:	Wet wall electrostatic precipitators.
Control Equipment Operating Parameters:	Secondary volts, primary amperes, spark rates and water flow.
Rationale for Worst Case:	None.
Normal Operating Range:	93,000 ACFM @ 150° F.
Air Pollution Control & Process Monitoring:	Fuel usage and tons processed during test period will be recorded as will the operating parameters for the WWESP.

PART IV TEST METHODS

- A. EPA Method 1 for the location of sampling ports and points. Location of the sampling ports must be approved before the test.

- B. EPA Method 2 for velocity and volumetric flow rate. Three determinations: one measurement concurrently with each test run for pollutant.
- C. EPA Method 3. Three determinations; one measurement on an integrated sample taken concurrently with each test run for pollutant.
- D. EPA Method 4 for the determination of moisture in the flue gases. Three determinations: one measurement concurrently with each test for pollutant.
- E. EPA Method 5 for the determination of particulate matter. Three one-hour determinations will be performed. Condensible compounds will be collected during each determination and analyzed as per MN Rules Part 7005.0500. Results will be reported both as total particulate matter containing condensibles and total particulate matter excluding condensibles.
- F. EPA Method 6C for the determination of sulfur dioxide. Three one-hour monitors will be performed.
- G. EPA Method 7E for the determination of nitrogen oxides. Three one-hour monitorings will be performed.
- H. EPA Method 9 as amended by Minnesota Rules Part 7006.1860 for the Determination of Opacity. Two hundred forty (240) observations during a one-hour period concurrent with one of the test runs by a certified reader.

PART V. CEMS RELATIVE ACCURACY

NA

PART VI. OTHER

- A. Pollutants will be reported as GR/DSCF and LB/HR.
- B. Description and date of last maintenance work done before the test. This information will be supplied as a part of the test report.
- C. One complete test report will be submitted within 45 days after the date of the test.
- D. One microfiche copy of the report will be submitted within 105 days after the date of the test.