

AP-42 Section 11.28
Reference 11
Report Sect. B20
Reference 13

Note: This is a reference cited in AP 42, *Compilation of Air Pollutant Emission Factors, Volume I Stationary Point and Area Sources*. AP42 is located on the EPA web site at www.epa.gov/ttn/chief/ap42/

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**PARTICULATE EMISSIONS
TEST REPORT
FOR
W. R. GRACE
AUGUST 1991**



RTP ENVIRONMENTAL ASSOCIATES INC.

AIR • WATER • SOLID WASTE CONSULTANTS

**PARTICULATE EMISSIONS
TEST REPORT
FOR
W. R. GRACE
AUGUST 1991**

PREPARED BY:

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INTRODUCTION

INTRODUCTION

This report presents the final results of the emissions tests performed for W.R. Grace.

The purpose of the tests was to determine the particulate emissions of the unit. The results of the tests can be found in Section II of this report.

The emissions testing was performed by Total Source Analysis, Inc., whose main office is located at 139 W. Herrick, Wellington, Ohio.

The tests were performed on August 27/29, 1991. The testing was performed in accordance with EPA reference methods as published in the July 1, 1990 Federal Register, - "Standards of Performance for New Stationary Sources" and subsequent revisions.

The testing equipment and sampling procedures are described in Section III of this report. The raw field data and equations used in determining final results are presented in the Appendix.

SUMMARY OF TEST RESULTS

SUMMARY OF TEST RESULTS

The following charts present the results of the particulate emissions tests performed at W.R. Grace.

PARTICULATE

RUN #	DATE	LOCATION	DSCFM	LB/DSCF	LBS/HOUR
1	8-27-91	Dryer Stack	19,644	1.21E-05	14.30
2	8-27-91	Dryer Stack	19,461	1.49E-05	17.43
3	8-27-91	Dryer Stack	19,586	1.74E-05	20.48
AVG.			19,564	1.48E-05	17.40

RUN #	DATE	LOCATION	DSCFM	LB/DSCF	LBS/HOUR
4	8-28-91	West Stack	4,462	2.34E-05	6.27
5	8-28-91	West Stack	4,533	2.14E-05	5.83
6	8-28-91	West Stack	4,606	2.60E-05	7.19
AVG.			4,534	2.36E-05	6.43

RUN #	DATE	LOCATION	DSCFM	LB/DSCF	LBS/HOUR
7	8-28-91	East Stack	4,595	1.11E-05	3.06
8	8-28-91	East Stack	4,411	9.13E-06	2.41
9	8-28-91	East Stack	4,444	1.60E-05	4.29
AVG.			19,564	1.21E-05	3.25

RUN #	DATE	LOCATION	DSCFM	LB/DSCF	LBS/HOUR
10	8-29-91	Unit 4 Stack	1,860	9.21E-06	1.02
11	8-29-91	Unit 4 Stack	1,908	1.27E-05	1.45
12	8-29-91	Unit 4 Stack	1,928	1.82E-05	2.10
AVG.			1,899	1.34E-05	1.52

Total Source Analysis, Inc.
Particulate Test Analysis

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Run Number	1	2	3
Data set	(01)	(02)	(03)
Date	8-27-91	8-27-91	8-27-91
Location	DRYER	DRYER	DRYER
	STACK	STACK	STACK
Start time	10:40	13:00	14:35
End time	11:45	14:03	15:15
Barometric Pressure	In. Hg 29.65	29.65	29.65
Static Pressure	In. H2O 1.20	1.20	1.20
Volume of Condensate	Mls 275	290	309
Volume Sampled	DCF 50.847	50.809	55.231
Meter Correction Factor	1.02	1.02	1.02
Square Root of Delta P	1.306	1.308	1.315
Orifice Pressure	In. H2O 2.62	2.92	2.91
Meter Temperature	Deg. F 89	92	97
Flue Temperature	Deg. F 174	175	176
Percent CO2	% 0.00	0.00	0.00
Percent O2	% 20.90	20.90	20.90
Diameter of Nozzle	In 0.225	0.225	0.225
Area of Flue	Sq Ft 5.94	5.94	5.94
Sample Time	Min 60	60	60
Weight Gain	Grams 0.2737	0.3349	0.4212
Absolute Flue Pressure	In. Hg 29.74	29.74	29.74
Corrected Sample Volume	DSCF 49.73	49.46	53.28
Moisture in Flue Gas	% 20.7	21.6	21.4
Molecular Weight	Lb/LbMole 26.60	26.49	26.51
Velocity of Flue Gas	Fps 83.97	84.33	84.81
Volume of Flue Gas	ACFM 29,926	30,054	30,228
Volume of Flue Gas	DSCFM 19,644	19,461	19,586
Dust Concentration	Lb/DSCF 1.21E-05	1.49E-05	1.74E-05
Dust Concentration	Lbs/Hour 14.30	17.43	20.48
Dust Concentration	Grs/ACF 5.66E-02	6.89E-02	8.03E-02
Dust Concentration	Grs/DSCF 8.49E-02	.10	.12
Isokinetic Rate	% 90.6	91.0	97.4

Averages:

Stack Temperature : 175.0
Vol Flue Gas ACFM : 30.069
Part Emis Lb/DSCF : 1.48E-05
Grs/ACF : 6.86E-02
Lbs/MBtu : 0

Percent O2 : 20.9
DSCFM : 19.564
Lb/Hour : 17.40
Grs/DSCF : .10

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Particulate Test Analysis

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Run Number	4	5	6
Data set	(04)	(05)	(06)
Date	8-28-91	8-28-91	8-28-91
Location	WEST STACK	WEST STACK	WEST STACK
Start time	08:15	09:45	11:05
End time	09:15	10:47	12:07
Barometric Pressure	In. Hg 30.24	30.24	30.24
Static Pressure	In. H2O 0.80	0.80	0.80
Volume of Condensate	Mls 39	42	38
Volume Sampled	DCF 50.711	50.486	49.290
Meter Correction Factor	1.02	1.02	1.02
Square Root of Delta P	0.795	0.809	0.823
Orifice Pressure	In. H2O 2.60	2.62	2.49
Meter Temperature	Deg. F 82	85	90
Flue Temperature	Deg. F 110	109	113
Percent CO2	% 0.00	0.00	0.00
Percent O2	% 20.90	20.90	20.90
Diameter of Nozzle	In 0.254	0.254	0.254
Area of Flue	Sq Ft 1.77	1.77	1.77
Sample Time	Min 60	60	60
Weight Gain	Grams 0.5444	0.4939	0.5794
Absolute Flue Pressure	In. Hg 30.30	30.30	30.30
Corrected Sample Volume	DSCF 51.23	50.72	49.06
Moisture in Flue Gas	% 3.5	3.8	3.5
Molecular Weight	Lb/LbMole 28.46	28.43	28.46
Velocity of Flue Gas	FPS 46.41	47.22	48.13
Volume of Flue Gas	ACFM 4.929	5.015	5.117
Volume of Flue Gas	DSCFM 4.462	4.533	4.606
Dust Concentration	Lb/DSCF 2.34E-05	2.14E-05	2.60E-05
Dust Concentration	Lbs/Hour 6.27	5.83	7.19
Dust Concentration	Grs/ACF .15	.13	.16
Dust Concentration	Grs/DSCF .16	.15	.18
Isokinetic Rate	% 96.1	93.7	89.2

Averages:

Stack Temperature : 110.7
Vol Flue Gas ACFM : 5,020
Part Emis Lb/DSCF : 2.36E-05
Grs/ACF : .15
Lbs/MBtu : 0

Percent O2 : 20.9
DSCFM : 4,534
Lb/Hour : 6.43
Grs/DSCF : .16

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Particulate Test Analysis

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91-155

Run Number	7	8	9
Data set	(07)	(08)	(09)
Date	8-28-91	8-28-91	8-28-91
Location	EAST STACK	EAST STACK	EAST STACK
Start time	12:30	13:50	15:00
End time	13:34	14:51	16:02
Barometric Pressure	In. Hg 30.24	30.24	30.24
Static Pressure	In. H2O 0.70	0.70	0.70
Volume of Condensate	Mls 41	39	39
Volume Sampled	DCF 49.491	41.317	40.940
Meter Correction Factor	1.02	1.02	1.02
Square Root of Delta P	0.836	0.807	0.813
Orifice Pressure	In. H2O 2.49	1.72	1.70
Meter Temperature	Deg. F 93	95	100
Flue Temperature	Deg. F 131	132	131
Percent CO2	% 0.00	0.00	0.00
Percent O2	% 20.90	20.90	20.90
Diameter of Nozzle	In 0.232	0.232	0.232
Area of Flue	Sq Ft 1.77	1.77	1.77
Sample Time	Min 60	60	60
Weight Gain	Grams 0.2468	0.1686	0.2916
Absolute Flue Pressure	In. Hg 30.29	30.29	30.29
Corrected Sample Volume	DSCF 48.99	40.68	39.94
Moisture in Flue Gas	% 3.8	4.3	4.4
Molecular Weight	Lb/Lbmole 28.43	28.37	28.36
Velocity of Flue Gas	Fps 49.74	48.10	48.43
Volume of Flue Gas	ACFM 5,282	5,108	5,143
Volume of Flue Gas	DSCFM 4,595	4,411	4,444
Dust Concentration	Lb/DSCF 1.11E-05	9.13E-06	1.60E-05
Dust Concentration	Lbs/Hour 3.06	2.41	4.29
Dust Concentration	Grs/ACF 6.85E-02	5.59E-02	9.84E-02
Dust Concentration	Grs/DSCF 7.77E-02	6.39E-02	.11
Isokinetic Rate	% 107.0	92.5	90.2

Averages:

Stack Temperature : 131.3
Vol Flue Gas ACFM : 5,178
Part Emis Lb/DSCF : 1.21E-05
Grs/ACF : 7.43E-02
Lbs/MBtu : 0

Percent O2 : 20.9
DSCFM : 4.483
Lb/Hour : 3.25
Grs/DSCF : 8.48E-02

Total Source Analysis, Inc.
Particulate Test Analysis

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91-155

Run Number	10 (10)	11 (11)	12 (12)
Data set			
Date	8-29-91	8-29-91	8-29-91
Location	UNIT 4 STACK	UNIT 4 STACK	UNIT 4 STACK
Start time	08:00	09:20	10:45
End time	09:02	10:22	11:50
Barometric Pressure	In. Hg 30.16	30.16	30.16
Static Pressure	In. H2O 0.05	0.05	0.05
Volume of Condensate	Mls 33	26	32
Volume Sampled	DCF 43.769	45.292	45.333
Meter Correction Factor	1.02	1.02	1.02
Square Root of Delta P	0.324	0.332	0.340
Orifice Pressure	In. H2O 1.93	2.09	2.21
Meter Temperature	Deg. F 83	90	96
Flue Temperature	Deg. F 83	88	98
Percent CO2	% 0.00	0.00	0.00
Percent O2	% 20.90	20.90	20.90
Diameter of Nozzle	In 0.365	0.365	0.365
Area of Flue	Sq Ft 1.77	1.77	1.77
Sample Time	Min 60	60	60
Weight Gain	Grams 0.1836	0.2595	0.3672
Absolute Flue Pressure	In. Hg 30.16	30.16	30.16
Corrected Sample Volume	DSCF 43.95	44.92	44.48
Moisture in Flue Gas	% 3.4	2.7	3.3
Molecular Weight	Lb/LbMole 28.47	28.54	28.48
Velocity of Flue Gas	Fps 18.50	19.02	19.68
Volume of Flue Gas	ACFM 1,965	2,020	2,090
Volume of Flue Gas	DSCFM 1,860	1,908	1,928
Dust Concentration	Lb/DSCF 9.21E-06	1.27E-05	1.82E-05
Dust Concentration	Lbs/Hour 1.02	1.45	2.10
Dust Concentration	Grs/ACF 6.18E-02	8.49E-02	.11
Dust Concentration	Grs/DSCF 6.44E-02	8.91E-02	.12
Isokinetic Rate	% 95.8	95.4	93.5

Averages:

Stack Temperature : 89.7
Vol Flue Gas ACFM : 2,025
Part Emis Lb/DSCF : 1.33E-05
Grs/ACF : 8.85E-02
Lbs/MBtu : 0

Percent O2 : 20.9
DSCFM : 1.899
Lb/Hour : 1.53
Grs/DSCF : 9.36E-02

SAMPLING AND ANALYTICAL PROCEDURES

TESTING EQUIPMENT - EPA METHOD 5 SAMPLING TRAIN

A Nutech Corporation Stack Sampler was used at the sampling location(s). The particulate sampling train consisted basically of a glass or stainless steel probe; a variable-heat-controlled filter oven with a calibrated Type K (Chromel/Alumel) thermocouple located at the impinger outlet; a 1/2-hp shaft sealed carbon vane vacuum pump assembly with a vacuum gauge; a control unit with an elapse time indicator, a temperature selector switch, a temperature indicator (potentiometer), temperature controllers, gauges, a calibrated dry gas meter, and an umbilical and various interconnecting hoses, fitting and valves. An appropriately sized glass or stainless-steel nozzle, a calibrated Type K temperature sensor, a static pressure tube, a calibrated S type pitot tube and a variable-heat-controlled stainless-steel liner with a calibrated Type K (Chromel/Alumel) thermocouple are integral parts of the probe assembly.

The vacuum pump was used to control gas sampling rates. The control unit was used to control probe and oven temperatures. The control unit was also used to monitor elapsed sampling times, temperatures, velocities, static pressure, gas sampling rates and sampled gas volume.

Analyzer (Orsat)

Flue gas concentrations were determined with a Gas Analyzer (Orsat) which measures the percentage of carbon dioxide, percentage of oxygen and percentage of carbon monoxide to the nearest tenth of a percent.

Programmable Calculator

A Hewlett Packard, Model 32S, programmable calculator was used to determine the isokinetic sampling rate at each sampling point.

Prior to the field testing, the following procedures were performed: All instruments were checked and calibrated. Gelman Spectro Grade, glass-fiber-mat filters with 99.95 percent retention of 0.3-micron particles were individually numbered, placed in similarly numbered glass petri dishes, desiccated for 24 hours and weighed on a Sartorius analytical balance to the nearest 0.1-milligram, and weighed a minimum of every six hours until two consecutive weights within +0.5 milligram were obtained, or heated for two to three hours at 220 degrees F, cooled in a desiccator and weighed. Several 250 milliliter crucibles were desiccated for a minimum of 24 hours and weighed in the same manner as the filters and petri dishes. Also, several 200-gram quantities of Type 6-16 mesh indicating silica gel were weighed on an Ohaus beam balance and placed into separate airtight polypropylene storage bottles.

The number of sampling points and positions of the points in the flue at the sampling location(s), and the sampling time at each point were determined prior to the particulate testing. The sampling procedures were performed in accordance with the Environmental Protection Agency's Reference Method 5, "Determination of Particulate Emissions from Stationary Sources" in the July 1, 1990 Federal Register, "Standards of Performance for New Stationary Sources" and subsequent revisions.

Before each test run a particulate sampling train was prepared inpart at the sampling location(s) in the following manner: An appropriately sized sampling nozzle was installed onto the inlet of the sampling probe and capped. The probe was then dimensioned and marked with glass-cloth tape at increments that corresponded with the predetermined sampling positions in the flue. A standard impinger assembly was prepared by adding 100 milliliters of distilled water to each of the first two impingers. The third impinger was left dry and the fourth was filled with approximately 200 grams of type 6-16 mesh indicating silica gel. The entire impinger assembly was then placed in an ice bath. A disc filter was removed from its petri dish and placed inside of a filter holder. The filter holder was then placed inside of a filter oven and assembled to the sampling probe outlet and the impinger unit inlet. Next, an umbilical and sampling hoses were connected to the sampling probe, filter oven, impinger unit, a vacuum pump and the control unit, accordingly.

The probe and oven were then heated to and held at 248 degrees plus or minus 25 degrees.

As soon as the probe and oven temperatures had stabilized the entire sampling train assembly was leak-checked at a minimum of 15 inches of mercury vacuum for one minute and the leakage rate recorded. A leakage rate of less than .02 cfm and no vacuum loss was considered acceptable.

After the particulate sampling train had been assembled, the probe and oven heated, and the entire system leak-checked, as previously described, the particulate sampling was performed.

Three test runs were performed at the sampling location(s). The sampling data for each test run was recorded on a field test form during each of the sampling periods.

After the completion of a test run, the following procedures were performed: A final leak-check was performed at maximum vacuum or greater incurred during the test for one minute and the leakage rate recorded. The flue gas moisture collected in the first three impingers was measured and recorded. The moisture laden silica gel in the fourth impinger was transferred to an appropriately marked, airtight polypropylene bottle and retained for later weighing. The weight gain of the silica gel moisture collection was added to the measured moisture condensed for that test run. The sample nozzle, probe and filter holder were capped and taken to a clean area for sample recovery. At the recovery area, the disc filter was carefully removed from the filter holder and transferred to its petri dish for later weighing.

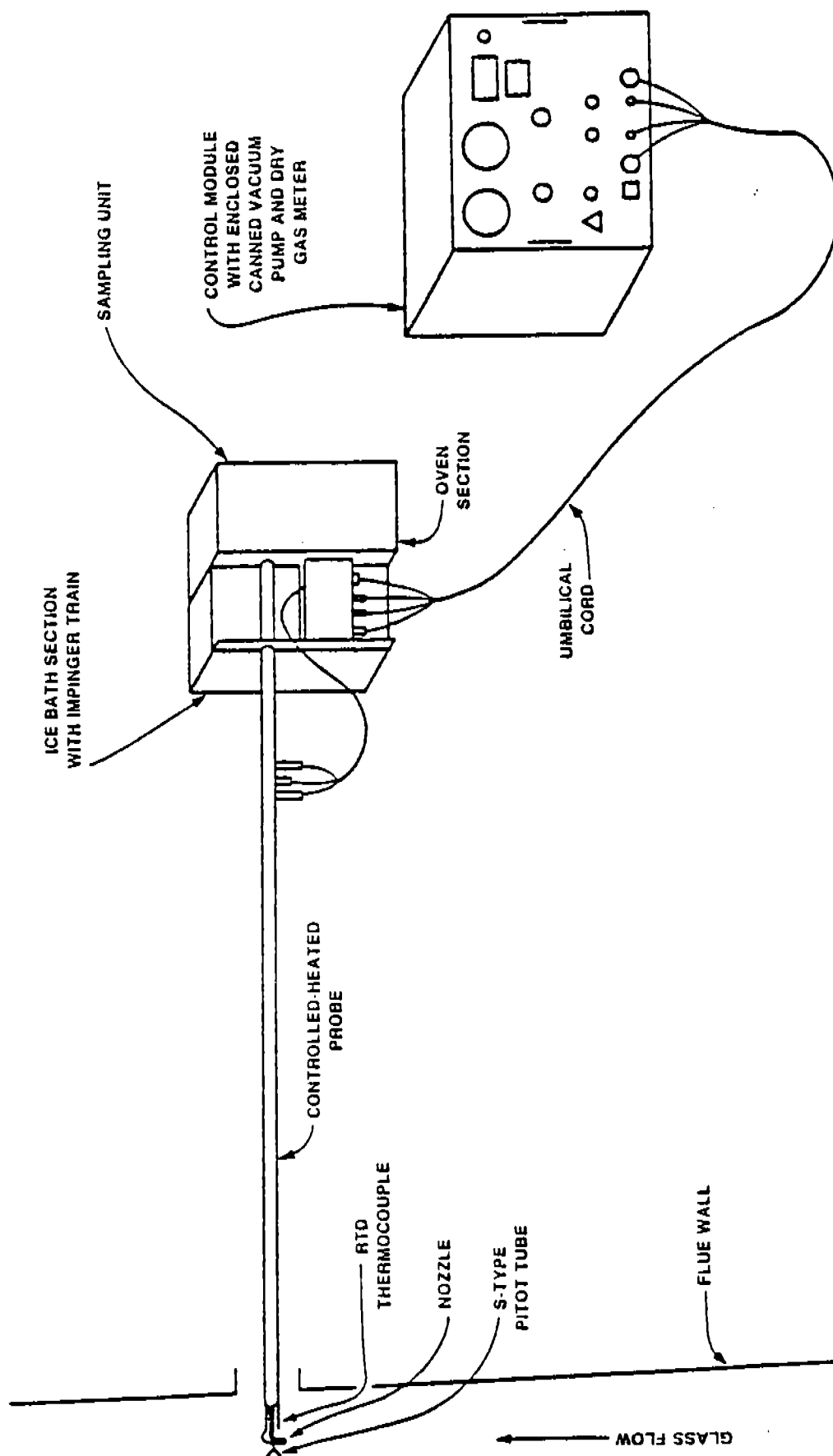
The sampling nozzle, probe and filter holder were washed with nanograde acetone, glass components were washed three times, stainless steel components were washed six times and visually inspected for cleanliness. The acetone washing and acetone blank were collected and labeled polypropylene sample bottles and retained for later evaporation, desiccation and weighing.

Flue gas concentrations (percentage of CO_2 , percentage of O_2 , and percentage of CO) were determined by taking several Orsat samples of the gas collected, simultaneously with the particulate sampling, throughout the test run, by an integrated gas sampling train. The integrated gas sample was collected from the discharge of the particulate control unit. The sampling train was set at a predetermined constant flow rate to obtain an adequate sample or by taking direct readings from the sampling points. The concentrations for each test run were recorded on a field test form.

ANALYTICAL PROCEDURES - EPA REFERENCE METHOD 5 (PARTICULATE)

After the field testing was completed, the following procedures were performed: Each silica gel moisture collection was weighed in it's storage bottle on an Ohaus beam balance with sensitivity of 0.1-gram. Each disc filter and petri dish was oven dried at 220 degrees Fahrenheit for two to three hours and cooled in a dessicator for two hours before weighing. Each acetone washing and acetone blank was transferred from its sample bottle to a preweighed crucible for evaporation. When the acetone in a crucible had completely evaporated, the crucible was transferred to a desiccator for further drying at room temperature. Each acetone blank collected was used to determine the amount of residual weight each crucible retained due to acetone impurities. Each disc filter and petri dish, acetone washing and acetone blank was weighed on a Sartorius analytical balance with a sensitivity of 0.1-milligram.

All test instruments were recalibrated to determine the deviation percentage.



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TYPICAL
SAMPLING TRAIN

Sample Calculations

APPENDIX

NOMENCLATURE

acf = actual cubic feet
 acfm = actual cubic feet per minute
 A = effective area of flue in square feet
 acm = actual cubic meters
 acmm = actual cubic meters per minute
 A_n = inside area of sampling nozzle in square feet
 B_{ws} = water vapor in gas stream, proportion by volume
 %C = percent carbon by weight, dry basis
 %CO = percent carbon monoxide by volume, dry basis
 %CO₂ = percent carbon dioxide by volume, dry basis
 C_p = pitot tube coefficient
 D_i = dust loading per heat input in pounds (grams) per million Btu (calories) per Fr constant
 D_i' = dust loading per heat input in pounds (grams) per million Btu (calories) per Fr calculated
 dscf = dry standard cubic feet
 dscfh = dry standard cubic feet per hour
 dscm = dry standard cubic meters
 dscmh = dry standard cubic meters per hour
 fps = feet per second
 F_r = ratio factor of dry flue gas volume to heat value of combusted fuel in dry standard cubic feet (meters) per million Btu (calories)
 gms = grams
 gm-mole = gram-mole
 grs = grains
 ΔH = orifice pressure drop in inches water, average
 %H = percent hydrogen by weight, dry basis
 H_c = heat of combustion in Btu per pound, dry basis
 hr = hour
 %I = percent isokinetic
 in. Hg = inches mercury
 lbs = pounds
 lb-mole = pound-mole
 %M = percent moisture by volume
 mmBtu = million Btu
 mmcal = million calories
 mm Hg = millimeters mercury
 mps = meters per second
 M_s = molecular weight in pounds (gram) per pound (gram) mole (wet basis)
 %N = percent nitrogen by weight, dry basis
 %N₂ = percent nitrogen by difference, dry basis
 %O = percent oxygen by difference, dry basis
 %O₂ = percent oxygen by volume, dry basis
 P_b = barometric pressure in inches mercury
 P_{std} = standard absolute pressure (29.92 in Hg)
 P_s = absolute pressure in flue in inches (millimeters) mercury

P_f = static pressure in flue in inches water, average
 $\sqrt{\Delta P}$ = square root of velocity head in inches water, average
 %S = percent sulfur by weight, dry basis
 scf = standard cubic feet
 scm = standard cubic meters
 T_{std} = absolute temperature of air in degrees Rankine at standard conditions (528 degrees)
 T_s = absolute temperature of flue gas in degrees Rankin, average
 T_m = absolute temperature at meter in degrees Rankine, average
 V_s = velocity of flue gas in feet (meters) per second
 V_i = volume of condensate through the impingers in milliliters
 V_{lc} = volume of liquid collected in condenser in milliliters plus weight of liquid absorbed in silica gel in grams indicated as milliliters
 V_m = volume of metered gas measured at meter conditions in cubic feet (meters)
 V_{ms} = volume of metered gas corrected to dry standard conditions in cubic feet (meters)
 V_o = volume of flue gas at actual conditions in cubic feet (meters) per minute
 Q_{sd} = volume of flue gas corrected to dry standard conditions in cubic feet (meters) per hour
 V_t = total volume of flue gas sampled at actual conditions in cubic feet (meters)
 V_w = volume of water vapor in metered gas corrected to standard conditions in cubic feet (meters)
 V_{wc} = volume of water condensed in impingers corrected to standard conditions
 V_{wsg} = volume of water collected in silica gel corrected to standard conditions
 W_a = total weight of dust collected per unit volume in grains (grams) per actual cubic feet (meters)
 W_d = total weight of dust collected per unit volume in pounds (grams) per dry standard cubic feet (meters)
 W_g = total weight of dust collected in grams
 W_h = total weight of dust collected per unit volume in pounds (grams) per hour, dry basis
 W_p = total weight of dust collected in pounds
 W_s = total weight of dust collected per unit volume in grains (grams) per dry standard cubic feet (meters)
 W_{sg} = impinger silica gel weight gain in grams
 Y = metered gas volume correction factor
 Θ = total elapsed sampling time in minutes



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EPA DUST LOADING Formulas

- (1) ABSOLUTE FLUE PRESSURE (in. Hg)

$$P_s = (\pm P_f \div 13.6) + P_b$$

- (2) WATER VAPOR VOLUME IN METERED GAS CORRECTED TO STANDARD CONDITIONS (scf)

$$V_{wc} = .04707 \times V_l \quad V_{wsg} = .04715 \times W_{sg}$$

$$V_w = V_{wc} + V_{wsg}$$

- (3) METERED GAS VOLUME CORRECTED TO STANDARD CONDITIONS (scf)

$$V_{ms} = 17.64 \times Y \times V_m \frac{P_b + (\Delta H/13.6)}{T_m}$$

- (4) PERCENT MOISTURE IN FLUE GAS

$$B_{ws} = \frac{V_w}{(V_{ms} + V_w)} \%M = B_{ws} \times 100$$

- (5) AVERAGE RESULTS OF FLUE GAS ANALYSIS

$$\%N_2 \text{ dry} = 100 - (\%CO_2 + \%O_2 + \%CO)$$

- (6) APPROXIMATE MOLECULAR WEIGHT OF FLUE GAS (WET BASIS) (lb/lb-mole)

$$M_s = (18 \times B_{ws}) + ((.440 (\%CO_2) + .320 (\%O_2) + .280 (\%N_2 + \%CO)) \times (1 - B_{ws}))$$

- (7) GAS VELOCITY IN FLUE (fps)

$$V_s = 85.49 \times C_p \times (\sqrt{\Delta P}) \text{ avg. } \sqrt{\frac{T_s}{P_s \times M_s}}$$

- (8) FLUE GAS VOLUME AT ACTUAL CONDITIONS (acfm)

$$V_o = V_s \times A \times 60$$

- (9) FLUE GAS VOLUME CORRECTED TO DRY STANDARD CONDITIONS (dscfh)

$$Q_{sd} = \frac{T_{std}}{29.92} \times \frac{P_s}{T_s} \times V_o \times (1 - B_{ws}) \times 60$$

- (10) TOTAL FLUE GAS VOLUME SAMPLED AT ACTUAL CONDITIONS (acf)

$$V_t = \left[V_m \times Y \times \frac{T_s}{T_m} \times \left(\frac{P_b + (\Delta H/13.6)}{P_s} \right) \right] + \left(0.00267 \times V_{lc} \times \frac{T_s}{P_s} \right)$$



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EPA DUST LOADING FORMULAS (Continued)

(11) DUST CONCENTRATION FOR INDIRECT HEATING UNIT ACTUAL CONDITIONS AND STANDARD CONDITIONS

$$W_g = \text{gms}$$

$$W_p = 0.002205 \times W_g \text{ (lb)}$$

$$W_d = \frac{W_p}{V_{ms}} \text{ (lb/dscf)}$$

$$W_h = W_d \times Q_{sd} \text{ (lb/hr dry)}$$

$$W_a = \frac{7000 \times W_p}{V_t} \text{ (gr/acf)}$$

$$W_s = 7000 \times W_d \text{ (gr/dscf)}$$

$$D_l = \frac{9780 \times 20.9 \times W_d}{(20.9 - \%O_2)} \text{ (lb/mmBtu with constant 9780Fr)}$$

$$F_r = \frac{106 \times [(3.64 \times \%H) + (1.53 \times \%C) + (0.57 \times \%S) + (0.14 \times \%N) - (0.46 \times \%O)]}{H_c} \text{ (dscf/mmBtu)}$$

$$D_l' = \frac{20.9 \times W_d \times F_r}{(20.9 - \%O_2)} \text{ (lb/mmBtu with calculated } F_r)$$

(12) PERCENT OF ISOKINETIC SAMPLING

$$\%I = \frac{1.667 \times T_s \times \left\{ 0.00267 \times V_{lc} + \left[\frac{V_m \times Y}{T_m} \times (P_b + \Delta H/13.6) \right] \right\}}{\Theta \times V_s \times P_s \times A_n}$$



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Test Data Sheets

Particulate Field Data Sheet

Client W.R. GRACE (A.P.P.)						Date 8-28-91		Page 1 Of 2				
Project No. 91-155				Operator J. SUTTON		Orsat Analysis						
Sampling Location DRYER STACK				Run No. 1		CO ₂ + O ₂ O ₂ CO						
Filter No. 91-127		Acetone No.		Condensate 254 mL		0 20.9						
Barometric Pressure 29.65		Static Pressure +1.2		Probe Number 4-1								
Nozzle Diameter .228		Nozzle Number 2-4		Pilot Coefficient .84		Pilot Number 4-1						
Meter Corr. Factor 1.02		Meter-Orifice 10 (3.68)										
Sample Pt. Time 5 min		Assumed % Moisture 25%		Leak Test		Before 008 @ 15"		After 005 @ 10"				
Sample Point	ΔP	√ΔP	ΔH	Temperature °F						Vac. Pr (in. HG)	Dry Gas Meter Reading in Cu. Ft.	
				Stack	Probe	Imp. Out	Oven	Meter In	Meter Out			
START 10:40						66						121.916
A 1	1.4	1.183	2.11	180	259		254	8 4	1		125.45	
2	1.6	1.265	2.41	170	255		256	8 5	1		129.31	
3	1.8	1.342	2.79	166	255		261	8 8	1		133.62	
4	2.0	1.414	3.60	166	254		251	8 7	2		138.26	
5	1.8	1.342	2.79	179	255		256	8 8	2		142.78	
6	1.7	1.304	2.58	186	253		255	8 9	2		147.071	
B 1	1.7	1.304	2.58	164	254		256	8 9	2		151.26	
2	1.6	1.265	2.43	169	255		257	9 0	2		155.22	
3	1.7	1.304	2.63	164	252		258	9 0	2		159.95	
4	1.9	1.378	2.94	188	254		259	9 1	2		164.12	
5	1.8	1.342	2.78	177	253		252	9 1	2		168.79	
6	1.5	1.225	2.32	172	255		256	9 1	2		172.763	
STOP 11:45												
Ave 1.306 2.62 174								8 9			50.847	

Pilot Tube Leak Check: Before OK After OK
Integrated Bag Leak Check: Before OK After OK



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Particulate Field Data Sheet

Client W. R. GRACE						Date 8-27-91		Page 1 Of 2	
Project No. 91-155				Operator J. SUTTON		Orsat Analysis			
Sampling Location Dryer STACK						Run No. 2		CO ₂ + O ₂ O ₂ CO	
Filter No. 91-149		Acetone No.		Condensate 265		0 30.9			
Barometric Pressure 29.65		Static Pressure 1.2		Probe Number 4-1					
Nozzle Diameter .225		Nozzle Number 2-6		Pitot Coefficient .84		Pitot Number 4-1			
Meter Corr. Factor 1.02		Meter-Orifice 10		3.68					
Sample Pt. Time 5 min		Assumed % Moisture 22.70		Leak Test		Before 006 @ 15"		After 204 @ 10"	

Sample Point	ΔP	$\sqrt{\Delta P}$	ΔH	Temperature °F						Vac. Pr (in. HG)	Dry Gas Meter Reading in Cu. Ft.	
				Stack	Probe	Imp. Out	Oven	Meter In	Meter Out			
	START	1:00 pm				668						173.421
A 1	1.5	1.225	2.51	162	255		257	90	1		177.563	
2	1.6	1.265	2.75	158	256		257	90	1		181.872	
3	1.8	1.342	3.10	170	259		256	92	2		186.43	
4	2.0	1.414	3.43	166	258		257	92	2		191.18	
5	1.7	1.304	2.93	190	256		258	92	2		195.58	
6	1.6	1.265	2.66	185	257		255	92	2		199.831	
1	1.6	1.265	2.66	174	258		257	92	3		204.13	
2	1.8	1.342	2.99	178	256		256	92	2		209.73	
3	1.7	1.304	3.73	183	257		255	93	2		214.79	
4	2.1	1.449	3.52	184	255		257	93	3		219.36	
5	1.8	1.342	3.02	169	256		256	95	3		224.23	
6	1.4	1.183	2.35	178	255		251	95	3			
STOP 2:03 pm.												
AVG 1.308 2.92 175 92 50.809												

Pitot Tube Leak Check: Before OK After OK
 Integrated Bag Leak Check: Before OK After OK



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Particulate Field Data Sheet

Client W. R. GRACE (ATP)					Date 8-28-91					Page 1 of 2			
Project No. 91-155				Operator J. SUTTON				Orsat Analysis					
Sampling Location Dryer STACK						Run No. 3		CO ₂ + O ₂ O ₂ CO					
Filter No. 91-097		Acetone No.		Condensate 255 ML		C		20.9					
Barometric Pressure 29.65			Static Pressure 1.2		Probe Number 4E-1								
Nozzle Diameter .225		Nozzle Number 2-6		Pitot Coefficient .84		Pitot Number 4-1							
Meter Corr. Factor 1.02				Meter-Orifice 10 (3.68)									
Sample Pt. Time 5 min			Assumed % Moisture 25%			Leak Test Before 0040458 After 1-2012"							

Sample Point	ΔP	√ΔP	ΔH	Temperature °F						Vac. Pr (in. HG)	Dry Gas Meter Reading in Cu. Ft.	
				Stack	Probe	Imp. Out	Oven	Meter In	Meter Out			
	START	2:35				668						229.320
A 1	1.5	1.225	2.51	163	250		258	9.5	1		233.45	
2	1.8	1.342	3.02	178	252		257	9.5	2		237.99	
3	1.7	1.304	2.85	171	254		256	9.6	2		242.68	
4	1.9	1.378	3.18	184	256		259	9.6	2		249.93	
5	1.8	1.342	3.02	182	257		256	9.7	2		253.46	
6	1.6	1.265	2.68	169	256		259	9.8	2		257.739	
B 1	1.6	1.265	2.68	174	258		256	9.8	2		262.38	
2	1.7	1.304	2.85	175	256		259	9.7	3		266.90	
3	1.4	1.183	2.35	193	255		256	9.8	3		270.89	
4	2.1	1.449	3.52	175	254		258	9.8	3		275.85	
5	2.0	1.414	3.35	172	255		256	9.8	3		280.331	
6	1.7	1.304	2.85	178	256		253	9.9	3		284.55	
	STOP	3:45										
	AUG	1.315	2.91	176				9.7				55.231

Pitot Tube Leak Check: Before OK After OK
Integrated Bag Leak Check: Before OK After OK



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Particulate Field Data Sheet

Client <u>W. R. GRACE (RTP)</u>						Date <u>8-28-91</u>		Page <u>1</u> of <u>2</u>				
Project No. <u>91-155</u>			Operator <u>J. SUTTON</u>			Orsat Analysis						
Sampling Location <u>ROOF CYCLONE WEST STACK</u>			Run No. <u>4</u>			CO ₂	+ O ₂	O ₂	CO			
Filter No. <u>91-251</u>		Acetone No.		Condensate <u>25mL</u>		<u>0</u>		<u>20.9</u>				
Barometric Pressure <u>30.24</u>			Static Pressure <u>.8</u>		Probe Number <u>4-1</u>							
Nozzle Diameter <u>.254</u>		Nozzle Number		Pitot Coefficient <u>.84</u>		Pitot Number <u>4-1</u>						
Meter Corr. Factor <u>1.02</u>			Meter-Orifice <u>10 (3.68)</u>									
Sample Pt. Time <u>5 min</u>			Assumed % Moisture <u>8%</u>			Leak Test Before <u>003 @ 15"</u>		After <u>004 @ 12"</u>				
Sample Point	ΔP	$\sqrt{\Delta P}$	ΔH	Temperature °F						Vac. Pr (in. HG)	Dry Gas Meter Reading in Cu. Ft.	
				Stack	Probe	Imp. Out	Oven	Meter In	Meter Out			
	START	8:15				268						285.062
A 1	.65	.806	2.68	109	256		254	8	0	1		289.33
2	.75	.866	3.10	110	257		256	8	0	2		293.92
3	.73	.854	2.99	110	255		253	8	1	2		298.48
4	.66	.812	2.70	110	254		256	8	1	2		303.08
5	.59	.768	2.41	110	255		257	8	0	2		307.15
6	.53	.728	2.17	110	259		256	8	1	2		310.96
D 1	.70	.837	2.86	111	259		258	8	2	3		315.38
2	.72	.849	2.95	112	257		256	8	2	3		319.85
3	.70	.837	2.86	112	258		257	8	2	3		324.26
4	.62	.787	2.54	111	254		255	8	3	4		328.44
5	.55	.742	2.25	110	255		253	8	4	4		332.35
6	.42	.648	1.72	110	254		253	8	4	4		335.77
	STOP	9:15										
	AUG	.795	2.60	110				8	2			50.711

Pitot Tube Leak Check: Before OK After OK
 Integrated Bag Leak Check: Before OK After OK



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Particulate Field Data Sheet

Client W. R. GRACE (RPT)						Date 8-28-90		Page 1 of 2				
Project No. 91-155				Operator J. SUTTON		Orsat Analysis						
Sampling Location CYCLONE WEST STACK				Run No. 5		CO ₂ + O ₂ O ₂ CO						
Filter No. 91-138		Acetone No.		Condensate 25m		6. 20.9						
Barometric Pressure 30.24		Static Pressure +.8		Probe Number 4-1								
Nozzle Diameter .254		Nozzle Number		Pitot Coefficient .84		Pitot Number 4-1						
Meter Corr. Factor 1.02		Meter-Orifice 10 (3.68)										
Sample Pt. Time 5:11N		Assumed % Moisture 7%		Leak Test 006 @ 15"		Before 004 @ 12"		After				
Sample Point	ΔP	$\sqrt{\Delta P}$	ΔH	Temperature °F						Vac. Pr (in. HG)	Dry Gas Meter Reading in Cu. Ft.	
				Stack	Probe	Imp. Out	Oven	Meter In	Meter Out			
	START	9:15				264						336.553
D 1	.60	.775	2.45	108	254		259	83	1		340.63	
2	.69	.831	2.82	110	256		258	83	1		345.02	
3	.63	.794	2.58	111	258		256	84	2		349.27	
4	.75	.866	3.07	109	259		257	84	2		353.82	
5	.62	.787	2.54	108	255		253	85	2		357.93	
6	.55	.742	2.25	109	255		256	85	2		361.821	
A 1	.59	.768	2.41	108	251		256	86	3		365.83	
2	.77	.877	3.15	109	255		254	86	3		370.48	
3	.75	.866	3.07	108	254		251	86	3		375.05	
4	.70	.837	2.56	109	257		256	87	3		379.22	
5	.68	.825	2.49	109	256		258	87	3		383.34	
6	.55	.742	2.01	107	255		251	87	3		387.039	
	STOP	10:47										
	Avg	.809	2.62	109				85			50.486	

Pitot Tube Leak Check: Before OK
 Integrated Bag Leak Check: Before OK

After OK
 After OK



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Particulate Field Data Sheet

Client										Date		Page	
Project No.										Operator		Orsat Analysis	
Sampling Location										Run No.		CO ₂ + O ₂ O ₂ CO	
Filter No.										Acetone No.		Condensate	
Barometric Pressure										Static Pressure		Probe Number	
Nozzle Diameter										Nozzle Number		Pitot Coefficient	
Meter Corr. Factor										Meter-Orifice			
Sample Pt. Time										Assumed % Moisture		Leak Test	
Sample Pt.										Before		After	
Sample Point	ΔP	√ΔP	ΔH	Stack	Probe	Imp. Out	Oven	Meter In	Meter Out	Vac. Pr (in. HG)	Dry Gas Meter Reading in Cu. Ft.		
START 11:05													
A 1	.63	.794	2.30	112	254	1	256	89	2	387.23			
2	.71	.843	2.59	112	256	1	259	89	2	391.19			
3	.75	.866	2.74	113	257	1	260	91	2	395.36			
4	.78	.883	2.85	112	251	1	255	91	2	399.68			
5	.64	.800	2.34	111	254	1	256	91	2	404.09			
6	.52	.721	1.90	112	253	1	254	90	2	408.09			
STOP 12:07													
Ave. 823 2.44 113 41 44.290													

Pitot Tube Leak Check: Before
Integrated Bag Leak Check: Before

After 0.5
After 0.5



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Particulate Field Data Sheet

Client W. R. GRACE APP										Date 8-28-91 Page 1 of 2		
Project No. 91-155				Operator J. SATTON				Orsat Analysis				
Sampling Location CYCLONE EAST STACK						Run No. 7		CO ₂		+ O ₂	O ₂	CO
Filter No. 91-193		Acetone No.		Condensate				0		20.9		
Barometric Pressure 30.24				Static Pressure .7		Probe Number 4-1						
Nozzle Diameter .254		Nozzle Number		Pitot Coefficient .84		Pitot Number 4-1						
Meter Corr. Factor 1.02				Meter-Orifice 10 (3.68)								
Sample Pt. Time 5m.n				Assumed % Moisture 770		Leak Test		Before 0058 @ 15"		After 0038 @ 7"		

Sample Point	ΔP	√ΔP	ΔH	Temperature °F						Vac. Pr (in. HG)	Dry Gas Meter Reading in Cu. Ft.
				Stack	Probe	Imp. Out	Oven	Meter In	Meter Out		
	START	12:30				668					437.08
1A	.68	.825	2.49	127	254		255	9	1	2	441.19
2	.59	.768	2.09	130	256		251	9	1	2	444.98
3	.75	.866	2.66	131	255		257	9	2	2	449.26
4	.78	.883	2.77	131	254		257	9	2	2	453.60
5	.73	.854	2.59	134	250		254	9	2	2	457.80
6	.76	.872	2.70	131	251		253	9	3	2	462.08
1B	.65	.806	2.31	130	252		255	9	3	3	466.04
2	.70	.837	2.48	131	256		252	9	3	3	470.15
3	.75	.866	2.66	131	258		257	9	4	4	474.40
4	.68	.825	2.41	131	256		256	9	4	4	478.49
5	.70	.837	2.48	131	257		258	9	4	3	482.60
6	.62	.794	2.24	132	251		248	9	4	3	486.57
SOP 1:34											
DUE .836 2.49 131 9 3 489.49											

Pitot Tube Leak Check: Before

Integrated Bag Leak Check: Before



Total Source Analysis, Inc.
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Particulate Field Data Sheet

Client W. R. GRACE (RTP)						Date 8-28-91		Page 1 of 2		
Project No. 91-155			Operator J. SUTTON			Orsat Analysis				
Sampling Location CYCLONE EAST STACK					Run No. 8		CO ₂	+ O ₂	O ₂	CO
Filter No. 91-275		Acetone No.		Condensate						
Barometric Pressure 30.24			Static Pressure 1.7		Probe Number 4-1					
Nozzle Diameter .251		Nozzle Number		Pitot Coefficient .84		Pitot Number 4-1				
Meter Corr. Factor 1.02			Meter-Orifice 10 (3.68)							
Sample Pt. Time 5:11			Assumed % Moisture 7%			Leak Test		Before 005015"	After 004011"	

Sample Point	ΔP	$\sqrt{\Delta P}$	ΔH	Temperature °F						Vac. Pr (in. HG)	Dry Gas Meter Reading in Cu. Ft.
				Stack	Probe	Imp. Out	Oven	Meter In	Meter Out		
	START	1:50				668					489.075
D 1	.61	.791	2.16	131	258		263		93	1	492.87
2	.59	.768	1.51	132	254		257		93	2	496.08
3	.75	.866	1.92	133	256		253		94	2	499.72
4	.75	.866	1.92	133	251		248		95	2	503.36
5	.60	.775	1.53	133	256		251		95	3	506.53
6	.59	.768	1.51	131	254		253		95	3	509.73
A 1	.71	.843	1.81	129	256		254		95	2	513.38
2	.66	.812	1.64	129	257		256		95	2	516.78
3	.63	.794	1.61	131	252		253		95	3	520.08
✓ 4	.78	.883	1.99	130	251		252		96	3	523.78
5	.62	.787	1.58	131	252		254		96	3	527.28
6	.55	.742	1.41	131	253		252		95	2	530.39
	STOP	2:51									
	41°C	.807	1.72	132					95		41.317

Pitot Tube Leak Check: Before OK After OK
Integrated Bag Leak Check: Before OK After OK



Total Source Analysis, Inc.
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Particulate Field Data Sheet

Client W.R. GRACE						Date 8-28-91		Page 1 of 2			
Project No. 91-155				Operator J. SUTTON		Orsat Analysis					
Sampling Location CYCLONE EAST STACK				Run No. 9		CO ₂ + O ₂ O ₂ CO					
Filter No. 91-		Acetone No.		Condensate		0 20.9					
Barometric Pressure 30.24		Static Pressure .7		Probe Number 4-1							
Nozzle Diameter .254		Nozzle Number		Pitot Coefficient .84		Pitot Number 1-1					
Meter Corr. Factor 1.02		Meter-Orifice 10 (3.68)									
Sample Pt. Time 5 min		Assumed % Moisture 7		Leak Test		Before 205 @ 15"		After 206 @ 10"			
Sample Point	ΔP	$\sqrt{\Delta P}$	ΔH	Stack	Probe	Temp. °F Imp. Out	Oven	Meter In	Meter Out	Vac. Pr (in. HG)	Dry Gas Meter Reading in Cu. Ft.
START 3:00 pm											
A 1	.62	.787	1.58	126	254	258		9.8		2	534.14
2	.69	.831	1.80	133	255	259		9.8		2	537.93
3	.75	.866	1.95	136	255	258		9.9		3	541.68
4	.74	.860	1.90	134	256	257		9.9		3	545.26
5	.61	.781	1.56	134	258	255		10.0		3	548.53
6	.53	.728	1.36	135	259	256		10.0		2	551.59
B 1	.63	.794	1.61	132	254	258		10.0		2	554.93
2	.75	.866	1.92	130	251	256		10.0		2	558.53
3	.71	.843	1.82	129	254	257		10.1		2	562.05
4	.68	.825	1.74	127	255	253		10.1		3	565.49
5	.65	.806	1.67	125	252	250		10.1		3	568.85
6	.59	.768	1.51	128	250	254		10.1		3	572.654
STOP 4:02 pm											
Avg .813 1.70 131 100 41,940											

Pitot Tube Leak Check: Before **OK** After **OK**

Integrated Bag Leak Check: Before **OK** After **OK**



Total Source Analysis, Inc.
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Particulate Field Data Sheet

Client W. R GRACE (ATP)										Date		Page 1 Of 2	
Project No. 91-155				Operator J. Sutton						Orsat Analysis CO ₂ + O ₂ O ₂ CO 0 20.9			
Sampling Location UNIT 4 STACK								Run No. 10					
Filter No. 91-272		Acetone No.		Condensate 20 mL									
Barometric Pressure 30.16				Static Pressure .05		Probe Number 4-1							
Nozzle Diameter .365		Nozzle Number		Pitot Coefficient .84		Pitot Number 4-1							
Meter Corr. Factor 1.02				Meter-Orifice 10 (3.68)									
Sample Pt. Time 5 min				Assumed % Moisture 7%				Leak Test		Before After 006 @ 15" 004 @ 11"			
Sample Point	ΔP	$\sqrt{\Delta P}$	ΔH	Temperature °F						Vac. Pr (in. HG)	Dry Gas Meter Reading in Cu. Ft.		
				Stack	Probe	Imp. Out	Oven	Meter In	Meter Out				
	START	8:00				68						573.213	
A 1	.12	.346	2.17	79	252		258	7	8	1		577.23	
2	.15	.387	2.71	82	256		261	7	9	1		581.53	
3	.10	.316	1.81	84	257		260	7	9	2		585.06	
4	.13	.361	2.35	84	256		258	8	0	2		589.09	
5	.09	.300	1.63	86	257		256	8	0	3		592.46	
6	.07	.265	1.27	85	257		257	8	2	2		595.42	
D 1	.13	.361	2.35	82	254		257	8	4	2		599.43	
2	.12	.346	2.17	82	256		255	8	4	2		603.26	
3	.12	.346	2.17	84	256		259	8	5	2		607.10	
4	.10	.316	1.81	82	256		257	8	6	2		610.62	
5	.09	.283	1.45	83	255		256	8	6	2		613.77	
6	.07	.265	1.27	83	256		258	8	7	2		616.96	
STOP 9:02													
Avg .324 1.93 83 83 43.764													

Pitot Tube Leak Check: Before OK After OK
Integrated Bag Leak Check: Before OK After OK



Total Source Analysis, Inc.
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Particulate Field Data Sheet

Client <u>W. R. GRACE (RTP)</u>						Date <u>8-29-91</u>		Page <u>1</u> of <u>2</u>	
Project No. <u>91-155</u>				Operator <u>J. SUTTON</u>		Orsat Analysis			
Sampling Location <u>4 STACK</u>						Run No. <u>11</u>		CO ₂ + O ₂ O ₂ CO	
Filter No. <u>91-280</u>		Acetone No.		Condensate <u>18 mL</u>					
Barometric Pressure <u>30.16</u>		Static Pressure <u>0.05</u>		Probe Number <u>4-1</u>					
Nozzle Diameter <u>.365</u>		Nozzle Number		Pilot Coefficient <u>.84</u>		Pilot Number <u>4-1</u>			
Meter Corr. Factor <u>1.02</u>		Meter-Orifice <u>10 (3.68)</u>							
Sample Pt. Time <u>5 min</u>		Assumed % Moisture <u>7%</u>		Leak Test		Before <u>0.05 @ 15"</u>		After <u>0.05 @ 7"</u>	

Sample Point	ΔP	$\sqrt{\Delta P}$	ΔH	Temperature °F						Vac. Pr (in. HG)	Dry Gas Meter Reading in Cu. Ft.
				Stack	Probe	Imp. Out	Oven	Meter In	Meter Out		
	START 9:20					<68					617.931
D 1	.14	.374	2.53	88	254		256	8	7	3	622.09
2	.11	.332	1.99	88	256		258	8	8	3	625.73
3	.12	.346	2.17	89	256		255	8	8	2	629.58
4	.11	.332	1.99	89	257		256	9	0	2	633.29
5	.09	.300	1.72	89	256		254	9	0	2	636.74
6	.08	.283	1.53	90	251		252	9	0	2	639.98
A 1	.12	.346	2.29	87	256		259	9	1	3	643.92
2	.15	.387	2.87	88	257		256	9	1	3	648.39
3	.14	.374	2.68	88	255		256	9	1	3	652.68
4	.11	.332	2.10	88	256		258	9	2	3	656.88
5	.10	.316	1.91	88	254		252	9	2	4	660.19
6	.07	.265	1.34	89	248		253	9	1	3	663.22
	STOP 10:27										
	.16	.332	2.29	88				9	0		45.292

Pitot Tube Leak Check: Before OK After OK
Integrated Bag Leak Check: Before OK After OK



Total Source Analysis, Inc.
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Particulate Field Data Sheet

Client W. R. GRACE (RTP)						Date 8-29-91		Page 1 of 2			
Project No. 91-155				Operator J. SUTTON		Orsat Analysis					
Sampling Location UNIT 4 STACK				Run No. 12		CO ₂ + O ₂ O ₂ CO					
Filter No. 91-276		Acetone No.		Condensate 22 mL		1 20.9					
Barometric Pressure 30.16			Static Pressure .05		Probe Number 4-1						
Nozzle Diameter .365		Nozzle Number		Pitot Coefficient .84		Pitot Number 4-1					
Meter Corr. Factor 1.02			Meter-Orifice 10 (3.68)								
Sample Pt. Time 5:00 A.M.			Assumed % Moisture 5%			Leak Test 005 @ 1/4"		Before After 004 @ 1/4"			
Sample Point	ΔP	√ΔP	ΔH	Temperature °F						Vac. Pr (in. HG)	Dry Gas Meter Reading in Cu. Ft.
				Stack	Probe	Imp. Out	Oven	Meter In	Meter Out		
	START	10:45				268					664.190
A 1	.13	.361	2.49	88	251		252	9.3	1	667.08	
2	.15	.387	2.87	90	252		254	9.4	2	669.49	
3	.15	.387	2.87	90	253		253	9.4	2	675.92	
4	.12	.346	2.29	95	256		258	9.5	3	679.9.3	
5	.10	.316	1.91	98	257		256	9.5	3	683.52	
6	.09	.300	1.66	102	256		254	9.6	3	686.93	
D 1	.14	.374	2.58	103	254		256	9.6	3	691.123	
2	.12	.346	2.27	103	251		254	9.6	3	695.05	
3	.11	.332	2.08	102	251		254	9.7	3	698.82	
4	.11	.332	2.08	100	253		254	9.7	4	702.63	
5	.10	.316	1.99	102	250		251	9.7	4	706.22	
6	.08	.283	1.51	102	255		254	9.7	4	709.523	
	STOP	11:50									
AUG. 30 2.21				98				4.6		45.333	

Pitot Tube Leak Check: Before

Integrated Bag Leak Check: Before

After

After



Total Source Analysis, Inc.
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Calibration Sheets

Dry Gas Meter Calibration Sheet

Client 111 R 2/ace Run By TIM READER
 Project No. 91-155-04 Date 7-9-91
 Module 10 Barometric Press 29.43
 Orifice _____

STD P = 3.68

ΔH in. H ₂ O	Vw initial	Vw final	Vw ft. ³	Vd initial	Vd final	Vd ft. ³	tw °F	tdi °F	tdo °F	Pw in H ₂ O	Time @ min.
.5	262.020	265.940	3.920	708.353	712.258	3.905	79	86			10.0
1.0	266.167	271.635	5.468	712.483	717.942	5.459	79	87			10.0
2.0	271.765	279.305	7.540	718.070	725.524	7.514	79	89			10.0
4.0	279.589	290.195	10.606	725.860	736.422	10.562	79	91			10.0
6.0	290.452	303.438	12.976	736.673	749.522	12.849	79	92			10.0

ΔH	$\frac{\Delta H}{13.6}$	Mc (Y)	ΔH_a (For Small Orifice Only)	
		$\frac{Vw Pb (td + 460)}{Vd (Pb + \Delta H/13.6) (tw + 460)}$	$\frac{0.0317 \Delta H}{Pb (td + 460)}$	$\frac{(tw + 460) @^2}{Vw}$
.5	.0368	1.02	1.81649	
1.0	.0737	1.01	1.9134	
2.0	.147	1.02	2.0052	
4.0	.294	1.02	2.0195	
6.0	.441	1.02	2.0201	
Average		1.02	1.9646	

- ΔH = Orifice Setting
 Vw = Volume of Gas of Wet Test Meter
 Vd = Volume of Gas of Dry Gas Meter
 Pw = Pressure of Wet Test Meter
 tw = Temperature of Fluid in Wet Test Meter
 tdi = Inlet Temperature of Dry Gas Meter
 tdo = Outlet Temperature of Dry Gas Meter
 td = Average Temperature of Dry Gas Meter
 $@$ = Time required to pull specified cubic feet
 Mc = Dry Gas Meter Correction Factor
 ΔH_a = Orifice setting that would pull .75 cfm of air at standard conditions



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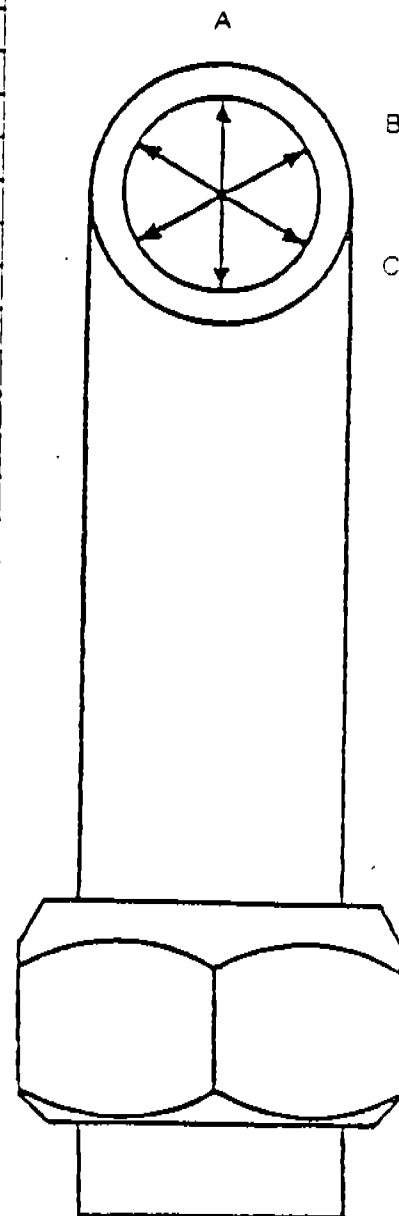
Nozzle Calibration

Sized By Bruce Woods

Notes

Date	Nozzle	Dimension			Difference	Avg. Diameter
		A	B	C		
7-9-91	Z-1	.188	.183	.137	.001	.139
	Z-2	.173	.173	.173	.000	.173
	Z-3	.175	.175	.175	.000	.175
	Z-4	.175	.175	.176	.001	.175
	Z-5	.175	.176	.176	.001	.176
	Z-6	.225	.226	.225	.001	.225
	Z-7	.254	.253	.254	.001	.254
	Z-8	.244	.245	.245	.001	.245
	Z-9	.248	.248	.248	.000	.248
	Z-10	.243	.244	.243	.001	.243
	Z-11	.282	.282	.283	.001	.282
	Z-12	.314	.314	.314	.000	.314
	Z-13	.313	.312	.313	.001	.313
	Z-14	.314	.314	.314	.000	.314
	Z-15	.321	.320	.320	.001	.320
	Z-16	.377	.377	.377	.001	.377
	Z-17	.369	.369	.370	.001	.369
	Z-18	.370	.371	.371	.001	.371
	Z-19	.365	.365	.365	.000	.365
	Z-20	.370	.370	.370	.000	.370
	Z-21	.364	.365	.365	.001	.365
	Z-22	.369	.370	.369	.001	.369
	Z-23	.485	.486	.485	.001	.485
	Z-24	.495	.495	.495	.000	.495
	Z-25	.494	.495	.495	.001	.495
	Z-26	.497	.498	.497	.001	.497
	Z-27	.594	.595	.595	.000	.595
	Z-28	.754	.755	.754	.001	.754
	Z-29	.759	.760	.761	.002	.760
	Z-30	.759	.760	.760	.001	.760
	Z-31	.495	.495	.495	.000	.495
	Z-32	.753	.759	.753	.001	.753
	Z-33	1.008	1.007	1.007	.001	1.007
	Z-34	1.024	1.025	1.025	.001	1.025
	Z-35	1.150	1.150	1.150	.000	1.150

All Dimensions are in inches.



Total Source Analysis, Inc.
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Laboratory Reports

Analytical Data Sheet

Client W. R. GRACEProject No. 91-155-0HDate 9/13/91

Run No. 1 (Dryer Stack)
 Filter No. 91-127
 Acetone No. 1
 Amount liquid lost during transport 0
 Acetone blank volume, ml 100
 Acetone wash volume, ml 200
 Acetone blank concentration, mg/mg (equation 5-4)** 3.8×10^{-6}
 Acetone wash blank, mg (equation 5-5)** 0.6

Container Number	Weight of Particulate Collected		
	Final Weight	Tare Weight	Weight Gain
1	0.4838	0.3491	0.1347
2	78.1106	77.9710	0.1396
3			
Less acetone blank			0.0006
Weight of particulate matter			0.2737

	Volume of Liquid Water Collected	
	Impinger Volume, ml	Silica Gel Weight, g
Final		271.2
Initial		250.0
Liquid collected		21.2
Total Volume Collected		271.2

Run No. 3
 Filter No. 91-097
 Acetone No. 3
 Amount liquid lost during transport 0
 Acetone blank volume, ml 100
 Acetone wash volume, ml 225
 Acetone blank concentration, mg/mg (equation 5-4)** 3.8×10^{-6}
 Acetone wash blank, mg (equation 5-5)** 0.7

Container Number	Weight of Particulate Collected		
	Final Weight	Tare Weight	Weight Gain
1	0.5162	0.3387	0.1775
2	66.4059	66.1615	0.2444
3			
Less acetone blank			0.0007
Weight of particulate matter			0.4212

	Volume of Liquid Water Collected	
	Impinger Volume, ml	Silica Gel Weight, g
Final		273.9
Initial		250.0
Liquid collected		23.9
Total Volume Collected		273.9

Run No. 2
 Filter No. 91-149
 Acetone No. 2
 Amount liquid lost during transport 0
 Acetone blank volume, ml 100
 Acetone wash volume, ml 190
 Acetone blank concentration, mg/mg (equation 5-4)** 3.8×10^{-6}
 Acetone wash blank, mg (equation 5-5)** 0.6

Container Number	Weight of Particulate Collected		
	Final Weight	Tare Weight	Weight Gain
1	0.5352	0.3496	0.1856
2	49.4205	49.2706	0.1499
3			
Less acetone blank			0.0006
Weight of particulate matter			0.3349

	Volume of Liquid Water Collected	
	Impinger Volume, ml	Silica Gel Weight, g
Final		274.7
Initial		250.0
Liquid collected		24.7
Total Volume Collected		274.7

Run No. Blank Acetone
 Filter No.
 Acetone No.
 Amount liquid lost during transport
 Acetone blank volume, ml 100
 Acetone wash volume, ml
 Acetone blank concentration, mg/mg (equation 5-4)** 3.8×10^{-6}
 Acetone wash blank, mg (equation 5-5)**

Container Number	Weight of Particulate Collected		
	Final Weight	Tare Weight	Weight Gain
1	67.4495	67.4492	0.0003
2			
3			
Less acetone blank			0.0003
Weight of particulate matter			0.0003

	Volume of Liquid Water Collected	
	Impinger Volume, ml	Silica Gel Weight, g
Final		
Initial		
Liquid collected		
Total Volume Collected		

*Convert weight of water to volume by dividing total weight increase by density of water (1g/ml): $\frac{\text{Increase, g}}{1\text{g/ml}} = \text{Volume Water, ml}$

**See Federal Register, Method 5, 6.6, & 6.7.

Analytical Data Sheet

Client W. R. GRACEProject No. 91-155-04Date 9/3/91

Run No. 4 (West Stack)
 Filter No. 91-251
 Acetone No. 4
 Amount liquid lost during transport 0
 Acetone blank volume, ml 100
 Acetone wash volume, ml 185
 Acetone blank concentration, mg/mg (equation 5-4)** 3.8×10^{-6}
 Acetone wash blank, mg (equation 5-5)** 0.6

Container Number	Weight of Particulate Collected		
	Final Weight	Tare Weight	Weight Gain
1	0.5117	0.3487	0.1630
2	80.4745	80.0925	0.3820
3			
Less acetone blank			0.0006
Weight of particulate matter			0.5444

	Volume of Liquid Water Collected	
	Iminger Volume, ml	Silica Gel Weight, g
Final		263.9
Initial		250.0
Liquid collected		13.9
Total Volume Collected		13.9 ml

Run No. 5
 Filter No. 91-132
 Acetone No. 5
 Amount liquid lost during transport 0
 Acetone blank volume, ml 100
 Acetone wash volume, ml 175
 Acetone blank concentration, mg/mg (equation 5-4)** 3.8×10^{-6}
 Acetone wash blank, mg (equation 5-5)** 0.5

Container Number	Weight of Particulate Collected		
	Final Weight	Tare Weight	Weight Gain
1	0.4951	0.3487	0.1464
2	63.9789	63.6309	0.3480
3			
Less acetone blank			0.0005
Weight of particulate matter			0.4939

	Volume of Liquid Water Collected	
	Iminger Volume, ml	Silica Gel Weight, g
Final		267.1
Initial		250.0
Liquid collected		17.1
Total Volume Collected		17.1 ml

Run No. 6
 Filter No. 91-234
 Acetone No. 6
 Amount liquid lost during transport 0
 Acetone blank volume, ml 100
 Acetone wash volume, ml 170
 Acetone blank concentration, mg/mg (equation 5-4)** 3.8×10^{-6}
 Acetone wash blank, mg (equation 5-5)** 0.5

Container Number	Weight of Particulate Collected		
	Final Weight	Tare Weight	Weight Gain
1	0.5262	0.3452	0.1810
2	75.4075	75.0086	0.3989
3			
Less acetone blank			0.0005
Weight of particulate matter			0.5794

	Volume of Liquid Water Collected	
	Iminger Volume, ml	Silica Gel Weight, g
Final		264.7
Initial		250.0
Liquid collected		14.7
Total Volume Collected		14.7 ml

Run No. _____
 Filter No. _____
 Acetone No. _____
 Amount liquid lost during transport _____
 Acetone blank volume, ml _____
 Acetone wash volume, ml _____
 Acetone blank concentration, mg/mg (equation 5-4)** _____
 Acetone wash blank, mg (equation 5-5)** _____

Container Number	Weight of Particulate Collected		
	Final Weight	Tare Weight	Weight Gain
1			
2			
3			
Less acetone blank			
Weight of particulate matter			

	Volume of Liquid Water Collected	
	Iminger Volume, ml	Silica Gel Weight, g
Final		
Initial		
Liquid collected		
Total Volume Collected		

*Convert weight of water to volume by dividing total weight increase by density of water (1g/ml); $\frac{\text{Increase, g}}{1\text{g/ml}} = \text{Volume Water, ml}$

**See Federal Register, Method 5, 6.6, & 6.7.

Analytical Data Sheet

Client W. R. GRACEProject No. 91-155-0HDate 9/3/91

Run No. 10 (4 STACK)
 Filter No. 91-272
 Acetone No. 10
 Amount liquid lost during transport 0
 Acetone blank volume, ml 100
 Acetone wash volume, ml 130
 Acetone blank concentration, mg/mg (equation 5-4)** 3.8×10^{-6}
 Acetone wash blank, mg (equation 5-5)** 0.4

Container Number	Weight of Particulate Collected		
	Final Weight	Tare Weight	Weight Gain
1	0.4123	0.3464	0.0659
2	109.9289	109.8108	0.1181
3			
Less acetone blank			0.0604
Weight of particulate matter			0.1836

	Volume of Liquid Water Collected	
	Impinger Volume, ml	Silica Gel Weight, g
Final		262.8
Initial		250.0
Liquid collected		12.8
Total Volume Collected		271 ml

Run No. 12
 Filter No. 91-276
 Acetone No. 12
 Amount liquid lost during transport 0
 Acetone blank volume, ml 100
 Acetone wash volume, ml 120
 Acetone blank concentration, mg/mg (equation 5-4)** 3.8×10^{-6}
 Acetone wash blank, mg (equation 5-5)** 0.4

Container Number	Weight of Particulate Collected		
	Final Weight	Tare Weight	Weight Gain
1	0.4702	0.3458	0.1244
2	106.3250	106.0818	0.2432
3			
Less acetone blank			0.0604
Weight of particulate matter			0.3672

	Volume of Liquid Water Collected	
	Impinger Volume, ml	Silica Gel Weight, g
Final		259.9
Initial		250.0
Liquid collected		9.9
Total Volume Collected		271 ml

Run No. 11
 Filter No. 91-280
 Acetone No. 11
 Amount liquid lost during transport 0
 Acetone blank volume, ml 100
 Acetone wash volume, ml 170
 Acetone blank concentration, mg/mg (equation 5-4)** 3.8×10^{-6}
 Acetone wash blank, mg (equation 5-5)** 0.5

Container Number	Weight of Particulate Collected		
	Final Weight	Tare Weight	Weight Gain
1	0.4165	0.3416	0.0749
2	106.5507	106.3657	0.1850
3			
Less acetone blank			0.0605
Weight of particulate matter			0.2595

	Volume of Liquid Water Collected	
	Impinger Volume, ml	Silica Gel Weight, g
Final		258.4
Initial		250.0
Liquid collected		8.4
Total Volume Collected		271 ml

Run No. _____
 Filter No. _____
 Acetone No. _____
 Amount liquid lost during transport _____
 Acetone blank volume, ml _____
 Acetone wash volume, ml _____
 Acetone blank concentration, mg/mg (equation 5-4)** _____
 Acetone wash blank, mg (equation 5-5)** _____

Container Number	Weight of Particulate Collected		
	Final Weight	Tare Weight	Weight Gain
1			
2			
3			
Less acetone blank			
Weight of particulate matter			

	Volume of Liquid Water Collected	
	Impinger Volume, ml	Silica Gel Weight, g
Final		
Initial		
Liquid collected		
Total Volume Collected		271 ml

*Convert weight of water to volume by dividing total weight increase by density of water (1g/ml); $\frac{\text{Increase, g}}{1\text{g/ml}} = \text{Volume Water, ml}$

**See Federal Register, Method 5, 6.6, & 6.7.

Analytical Data Sheet

Client W. R. GRACEProject No. 91-155-0HDate 9/3/91

Run No. 7 (Cyclone East Stack)
 Filter No. 91-193
 Acetone No. 7
 Amount liquid lost during transport 0
 Acetone blank volume, ml 100
 Acetone wash volume, ml 125
 Acetone blank concentration, mg/mg (equation 3-4)** 3.8×10^{-6}
 Acetone wash blank, mg (equation 3-5)** 0.4

Container Number	Weight of Particulate Collected		
	Final Weight	Tare Weight	Weight Gain
1	0.4219	0.3481	0.0738
2	102.7272	102.5538	0.1734
3			
Less acetone blank			0.0004
Weight of particulate matter			0.2468

	Volume of Liquid Water Collected	
	Iminger Volume, ml	Silica Gel Weight, g
Final		264.9
Initial		250.0
Liquid collected		14.9
Total Volume Collected		271 ml

Run No. 9
 Filter No. 91-277
 Acetone No. 9
 Amount liquid lost during transport 0
 Acetone blank volume, ml 100
 Acetone wash volume, ml 150
 Acetone blank concentration, mg/mg (equation 3-4)** 3.8×10^{-6}
 Acetone wash blank, mg (equation 3-5)** 0.4

Container Number	Weight of Particulate Collected		
	Final Weight	Tare Weight	Weight Gain
1	0.4021	0.3459	0.0562
2	98.9924	98.7616	0.2358
3			
Less acetone blank			0.0004
Weight of particulate matter			0.2916

	Volume of Liquid Water Collected	
	Iminger Volume, ml	Silica Gel Weight, g
Final		259.2
Initial		250.0
Liquid collected		9.2
Total Volume Collected		271 ml

Run No. 8
 Filter No. 91-275
 Acetone No. 8
 Amount liquid lost during transport 0
 Acetone blank volume, ml 100
 Acetone wash volume, ml 120
 Acetone blank concentration, mg/mg (equation 3-4)** 3.8×10^{-6}
 Acetone wash blank, mg (equation 3-5)** 0.4

Container Number	Weight of Particulate Collected		
	Final Weight	Tare Weight	Weight Gain
1	0.3764	0.3469	0.0295
2	102.7543	102.6148	0.1395
3			
Less acetone blank			0.0004
Weight of particulate matter			0.1686

	Volume of Liquid Water Collected	
	Iminger Volume, ml	Silica Gel Weight, g
Final		261.1
Initial		250.0
Liquid collected		11.1
Total Volume Collected		271 ml

Run No. _____
 Filter No. _____
 Acetone No. _____
 Amount liquid lost during transport _____
 Acetone blank volume, ml _____
 Acetone wash volume, ml _____
 Acetone blank concentration, mg/mg (equation 3-4)** _____
 Acetone wash blank, mg (equation 3-5)** _____

Container Number	Weight of Particulate Collected		
	Final Weight	Tare Weight	Weight Gain
1			
2			
3			
Less acetone blank			
Weight of particulate matter			

	Volume of Liquid Water Collected	
	Iminger Volume, ml	Silica Gel Weight, g
Final		
Initial		
Liquid collected		
Total Volume Collected		271 ml

*Convert weight of water to volume by dividing total weight increase by density of water (1g/ml): $\frac{\text{Increase, g}}{1\text{g/ml}} = \text{Volume Water, ml}$
 **See Federal Register, Method 3, 5.6, & 5.7.