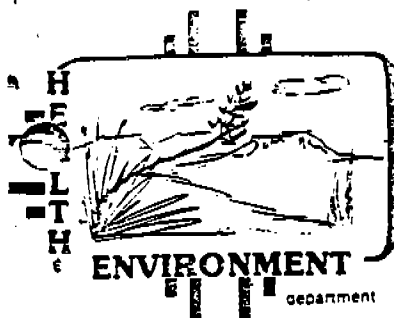


Note: This is a reference cited in *AP 42, Compilation of Air Pollutant Emission Factors, Volume I Stationary Point and Area Sources*. AP42 is located on the EPA web site at www.epa.gov/ttn/chief/ap42/

The file name refers to the reference number, the AP42 chapter and section. The file name "ref02_c01s02.pdf" would mean the reference is from AP42 chapter 1 section 2. The reference may be from a previous version of the section and no longer cited. The primary source should always be checked.



STATE OF NEW MEXICO

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AIR QUALITY SOURCE SAMPLING REPORT #198

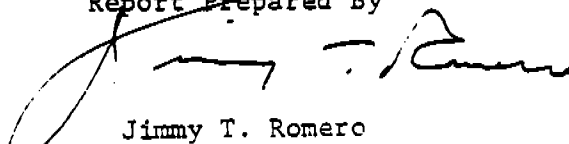
JOHNS MANVILLE PERLITE PLANT
DRYER AND MILL BAGHOUSE EXHAUSTS
TOTAL PARTICULATE
NO AGUA, NEW MEXICO

AP-42 Section	11.30
Reference	7
Report Sect.	4
Reference	4

ABSTRACT

On February 17, 18 and 19, 1981 the Johns Manville Perlite processing plant in No Agua was tested to determine total particulates exhausted from the dryer and mill baghouse. An average of three Method 5 runs from the dryer exhaust, show the plant to be emitting 3.89 lb/hr. One Rader test from each of the four mill baghouse exhausts, show the stacks to be emitting an average of 7.06 lb/hr which makes a total of 10.95 lb/hr of total particulates vented to the atmosphere. Air Quality Regulation 505 allows an emission rate of 34 lb/hr.

Report Prepared By


Jimmy T. Romero
Environmental Scientist III

Report Reviewed By

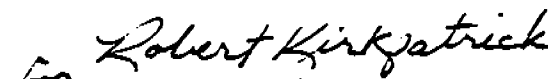

for Steve Schwebke
Assistant Engineer

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INTRODUCTION

1. Name and Address of Company Tested

Johns Manville Perlite Mill
No Agua, New Mexico
Antonito, Colorado 81120
Contact: J.A. Larson, Plant Manager
(303) 376-5666

2. Location of Plant Tested

The plant is located approximately 7 miles north of Tres Piedras on U.S. Highway 285.

3. Dates of Testing

February 17, 18 and 19, 1981

TEST PROCEDURES

1. Testing and Analytical Procedures (Dryer Stack)

Figure 3 shows a schematic of the sampling train. The procedures followed EPA Methods 1, 2 and 5 as described in Federal Register, Title 40, Part 60, Thursday, August 18, 1977. Method 1 was used for determining the number of traverse points across the duct. Method 2 was used in measuring the velocity of the stack gases and Method 5 was used in the collection of the particulate samples. In the procedures, particulate matter is withdrawn isokinetically from the source and collected on a glass fiber filter. The particulate mass which includes any material that condenses at or above the filtration temperature is determined gravimetrically after removal of uncombined water. Filters from the tests were desiccated and then weighed on a balance which measures accurately to the .00001 gram level. The particulate collected in the nozzle, probe and glassware prior to the filter are rinsed and the washings are analyzed at the Scientific Laboratory Division in Albuquerque, New Mexico. Analysis there includes evaporation of the liquid and weighing of the particulate residue.

2. Testing and Analytical Procedures (Mill Stacks)

a. Pre-test

Twenty-seven glass-fiber matte filters were desiccated for at least 48 hours before being weighed. Twenty-four of the filters were to be used in sampling while three were for determining any changes in tare weights. The sampler was washed with acetone, allowed to air-dry, and then was sealed before going to the test site.

At the site, a velocity profile of the stack was established using an S-type pitot tube. From the profile, an average velocity was determined for use in calculating the average stack gas flow rate. Determinations of CO₂ and O₂ content of the gas stream were made with fyrite combustion gas indicators. Moisture content was determined using wet bulb-dry bulb thermometers.

From the stack gas flow rate, the flow rate through the chosen nozzle was calculated so that isokinetic flow could be maintained. A sampling point was chosen which represented the average velocity head in the stack.

The probe was heated about 30 minutes prior to sampling to reduce condensation in the sampling train.

b. Rader Test

A preliminary run was made to check the assumed value for the orifice temperature. The orifice pressure drop was then adjusted to correct for changes in the orifice temperature in subsequent runs.

During each run, a preweighed filter was mounted in the heated sampler, the sampler was turned on, and the flow rate was adjusted. The sampler was then inserted into the stack gas stream at the same time that a stopwatch was started. When the flow could no longer be maintained at isokinetic conditions, the sampler and timer were stopped, and the train was removed from the stack. After removal from the stack, the soiled filter was removed and a new filter was inserted.

c. Post-test

After removal from the sampler, the filters were folded twice, with the collected material inside.

After the runs were completed, the sampler was cleaned. Probe and filter holder wash were taken to the Scientific Lab in Albuquerque. Filters were weighed to the nearest .0001 gram level at the Air Quality Lab after being desiccated for 48 hours.

3. Description of the Sampling Location (Dryer Baghouse)

Figure 2 shows a cross-section of the duct with the traverse and sample points for the dryer baghouse. The ports are located approximately 1.0 equivalent diameters upstream of the exhaust fan and 4.4 diameters downstream from any constriction to the flow.

4. Description of Sampling Location (Mill Baghouse)

Figure 4 shows a schematic of the stack tests. All four stacks were identical in size and area. The stacks were 39" by 37" in size. They are 10 feet from a constriction at the fan. The samples were taken at all four stack exits.

5. Personnel Conducting the Tests

Jimmy T. Romero - Environmental Scientist, III (Supervisor)
Mario Romero - Environmental Technician, III
Tim Booker - Environmental Technician, III

PROCESS DESCRIPTION

Perlite is a glassy volcanic rock consisting of oxides of silicone and aluminum combined as a natural glass by water of hydration. By a process called exfoliation, the material is rapidly heated to release water of hydration and thus to expand the spherules into low-density particles used primarily as aggregate in plaster, concrete or insulation.

The perlite ore in No Agua is mined from a quarry adjacent to the plant. It is then transferred by heavy trucks to the primary jaw crusher, which is then conveyed to secondary crushers. It is then stored in bins until the material is fed into two diesel fired dryers which removes surface moisture. The material is then milled, sized and transferred by truck to Antonito, Colorado.

Exhaust gases and particulates from the dryers are routed through dual cyclones to an Industrial Clean Air Baghouse. The dust collected from the baghouse is stored in dust bins, until it can be disposed of near the plant. Fugitive emissions collected, resulting from various process equipment, are routed through a separate baghouse comprised of five compartments.

RESULTS

The following table summarizes the results of the tests performed:

Johns Manville Perlite Plant

Date	2-17-81	2-18-81	2-19-81
Test Number	II	III	IV
Perlite Production Rate ton/hr.	85	85	80
Allowable Emission Rate lbs/hr.	34	34	34
Measured Emission Rate lbs/hr. (dryer)	4.55	4.24	2.87
Percent off Isokinetic Testing	95.70	96.60	97.10
Measured Emission Rate lbs/hr. (mill)		7.06	

Volume of gas sampled:

$$V_{(std)} = \frac{17.65 (V) (Mc) (Pb + \frac{\Delta H}{13.6})}{Tm + 460} = \text{scf (dry)}$$

Weight of particulate in stack gas:

$$Wg_{(std)} = .0154 \frac{W}{V_{(std)}} = \text{grains/scf (dry)}$$

Volume of moisture collected, if expressed as a vapor:

$$Vwv = .0474 (Vwf) = \text{scf}$$

Portion of stack gas volume which is moisture:

$$\% H_2O = \frac{100 (Vwv)}{V_{(std)} + Vwv} = \%$$

Fraction of stack gas volume which is dry:

$$F = \frac{100 - \% H_2O}{100} =$$

Molecular weight of dry stack gas:

$$Md = \% CO_2 (.44) + \% O_2 (.32) + \% N_2 (.28) = \text{lb./lb./mole}$$

Molecular weight of wet stack gas:

$$Mw = Md (F) + 18 (1-F) = \text{lb./lb. mole}$$

Absolute stack pressure:

$$Ps = Pb + \frac{Pg}{13.6} = \text{"Hg}$$

Velocity of the stack gas:

$$Vs = 5124 Cp \sqrt{\frac{\Delta P}{Ps Mw}} \sqrt{\frac{Ts + 460}{Ps Mw}} = \text{fpm}$$

Stack gas flow rate:

$$Q = Vs (A) = \text{acfm}$$

$$Q_{(std)} = \frac{17.65 (Vs) (A) (F) (Ps)}{Ts + 460} = \text{scfm (dry)}$$

Isokinetic sampling validation expression:

$$I = \frac{1039 (Ts + 460) V_{(std)}}{Vs (\pi) (Ps) (F) (Dn)^2} = \%$$

Particulate emission rate:

$$E = 8.6 \times 10^{-3} [Wg_{(std)}] [Q_{(std)}] = \text{lb./hr.}$$

CALCULATIONS

Mill Baghouse - Johns Manville

1. Moisture content of stack gas, wet bulb-dry bulb method:

$$T_s = \text{_____}^{\circ}\text{F}$$

$$T_w = \text{_____}^{\circ}\text{F}$$

From psychrometric chart, volume percent $\text{H}_2\text{O} = \text{_____}\%$

2. Molecular weight of stack gas:

$$M_w = 18 (X_{\text{H}_2\text{O}}) + \boxed{44} (X_{\text{CO}_2}) + 32 (X_{\text{O}_2}) + 28 (X_{\text{N}_2}) \boxed{1 - (X_{\text{H}_2\text{O}})} = \text{lb/lb mole}$$

_____ lb/lb mole

3. Velocity of stack gas:

$$V_s = 5124 \sqrt{\Delta p} C_p \sqrt{\frac{T_s + 460}{(P_s) (M_n)}} = \text{fpm}$$

4. Stack gas flow rate:

$$A = \frac{(D_s/12)^2}{4} \pi = \text{ft.}^2$$

$$A = W \times L = \text{ft.}^2$$

$$Q = V_s A$$

5. Isokinetic flow:

$$A_n = \frac{(D_n/12)^2}{4} \pi = \text{ft.}^2$$

For isokinetic sampling, $V_s = V_n$, so

$$Q_o = V_n A_n = V_s A_n = \text{_____ acfm}$$

$$(Q_o)_{\text{std}} = Q_o \left(\frac{60^{\circ} + 460^{\circ}}{T_s + 460} \right) = \text{_____ cfm}$$

From this flow at 60°F , an orifice ΔH can be chosen from curve 4 (see appendix) when the orifice temperature is known. The orifice temperature was assumed to be 60°F for the preliminary run and then determined from that run.

6. Particulate weight calculations:

a. W_{pr} = gross filter weight = filter tare weight

b. Adjusted particulate weight (including probe catch):

$$W_{aj} = \text{net filter wt.} + \left(\frac{\text{sample time}}{\text{total sample time}} \right) (W_{pr}) \pm \text{tare wt. change}$$

7. Emission rate:

a. $V_m = (t) (Q_o)$

b. $W_t = \left(\frac{W_{aj}}{V_m} \right) (Q) (K)$

TEST DATA

Test No.

		II	III	IV
V.....	Actual metered sample volume (CF)	48.46	49.88	47.5
P.....	Barometric pressure (Hg")	22.07	22.18	22.2
Tm.....	Average dry gas meter temp. (°F)	88	99.7	76
ΔH.....	Average pressure drop across orifice (H ₂ O")	.84	.97	.75
Mcf.....	Meter correction factor	.99	.99	.99
W.....	Total particulate collected (mg)	42.55	38.78	26.6
Vwf.....	Total H ₂ O collected from impingers (ML)	133	131	128
%CO ₂	Percent carbon dioxide in stack gas (dry)	1.0	2.0	2.0
%O ₂	Percent oxygen in stack gas (dry)	20.0	19.0	19.0
%N ₂	Percent nitrogen in stack gas (dry)	79.0	79.0	79.0
Pg.....	Stack pressure in stack	-.9	-.9	-8.5
Ts.....	Average stack gas temperature (°F)	180	180	180
Cp.....	S-type pitot tube correction factor	.83	.83	.83
√ΔP.....	Average square roots of velocity heads	.63	.63	.58
A.....	Area of stack (ft. ²)	20	20	20
t.....	Sample time (minutes)	72	72	72
Dn.....	Sampling nozzle diameter (inches)	.255	.255	.256

CALCULATED RESULTS

Ps.....	Absolute stack pressure ("Hg)	21.495	21.495	21.4
V _(std)	Corrected metered volume (SCF)	39.178	39.786	31.5
Wg _(std)	Weight of particulate in stack gas (grains/SCF)	.0189	.0175	.012
Vwv.....	Volume of water vapor collected (SCF)	6.304	6.209	6.06
%H ₂ O.....	Percent H ₂ O in stack gas by volume	15.6	15.15	16.1
F.....	Mole fraction of stack gas (dry)	.849	.849	.83
Md.....	Dry molecular wt. of stack gas (lb/lb-mole)	28.96	29.08	29.0
Mw.....	Wet molecular wt. of stack gas (lb/lb-mole)	27.25	27.416	27.2
Vs.....	Velocity of stack gas (FPM)	2803.96	2781.87	2512.
Q.....	Actual stack volumetric flow (ACFM)	56079	55637	5029
Q _(std)	Stack volumetric flow (SCFM)	27976	28194	2625
I.....	Percent isokinetics	95.7	96.6	97.1
E.....	Particulate emission rate (lb/hr.)	4.547	4.243	2.868

NOVENCLATUREMILL Baghouse

- A = Area of stack, ft.²
- A_n = Area of nozzle, ft.²
- V_m = Sample volume, ft.³
- C_p = Calibration factor, pitot tube, dimensionless
- ΔH = Pressure drop across orifice, inches H₂O
- ΔP = Velocity head, inches H₂O
- D_n = Diameter of sampling nozzle, inches
- D_s = Diameter of stack, inches
- K = Constant, .1323, $\frac{\text{min.} - \text{lb.}}{\text{hr. gram}}$
- % H₂O = % moisture in stack gas by volume
- M_w = Molecular weight of stack gas, (wet basis) lb./lb. mole
- P_b = Barometric pressure, inches Hg
- P_s = Absolute stack gas pressure, inches Hg
- Q_o = Flow through orifice at orifice temperature, cfm
- Q_o(std) = Flow through orifice at 60°F, fpm
- Q = Stack gas flow, acfm
- t = sample time, minutes
- T_o = Orifice temperature, °F
- T_s = Stack temperature, °F
- T_w = Wet bulb temperature, °F
- V_n = Velocity at nozzle, fpm
- V_s = Velocity of stack gas, fpm
- W_{aj} = Adjusted particulate weight, grams
- W_{pr} = Weight of particulate in probe washings, grams
- W_t = Emissions, lbs./hr.
- X_i = Mole fraction of component i, dimensionless

CALCULATIONS

mill) booghouse

Johns man oil

1. Moisture Content of Stack Gas, Wet Bulb-Dry Bulb Method:

$$T_s = \underline{62}^{\circ}\text{F}$$

$$T_w = \underline{50}^{\circ}\text{F}$$

From psychrometric chart, volume percent $\text{H}_2\text{O} = \underline{2.5}\%$

$$X_{\text{H}_2\text{O}} = \underline{\hspace{2cm}}$$

2. Molecular Weight of Stack Gas:

$$X_{\text{CO}_2} = \underline{0} \quad X_{\text{O}_2} = \underline{18\%} \quad X_{\text{N}_2} = \underline{82}$$

$$\text{Mw} = 18 (X_{\text{H}_2\text{O}}) + \frac{44(X_{\text{CO}_2}) + 32(X_{\text{O}_2}) + 28(X_{\text{N}_2})}{1 - (X_{\text{H}_2\text{O}})}$$

$$= 18 (2.5) + \frac{44(0) + 32(18) + 28(82)}{.98}$$

$$= \underline{29.5} \text{ lb./lb. mole}$$

3. Velocity of Stack Gas:

$$C_p = \underline{.53}$$

$$P_b = \underline{22.28} \text{ "Hg}$$

$$\Delta p = \underline{.73} \text{ "H}_2\text{O}$$

$$V_s = 5129 C_p \sqrt{\frac{(\Delta p)(T_s + 460)}{(P_b)(\text{Mw})}} = 5129 (.53) \sqrt{\frac{(.73)(512)}{(22.28)(29.5)}} = \underline{3355} \text{ fpm}$$

4. Stack Gas Flow Rate:

$$A = \frac{(D_s/12)^2}{4} \pi = \frac{(.12)^2}{4} \pi = \underline{10.02} \text{ ft.}^2$$

$$Q = V_s A = (3355)(10.02) = \underline{33617} \text{ acfm}$$

5. Isokinetic Flow:

$$D_n = \underline{1.75} \text{ inches}$$

$$A_n = \frac{(D_n/12)^2}{4} \pi = \frac{(.1458)^2}{4} \pi = \underline{.01039} \text{ ft.}^2$$

For isokinetic sampling, $V_s = V_n$, so

$$Q_o = V_n A_n = V_s A_n = (3355)(.01039) = \underline{34.85} \text{ acfm}$$

$$(Q_o)_{\text{std}} = Q_o \left(\frac{60^{\circ} + 460^{\circ}}{T_s + 460} \right) = (34.85) \left(\frac{520}{542} \right) = \underline{33.44} \text{ cfm}$$

From this flow at 60°F , an orifice ΔH can be chosen from Curve 4 (see appendix) when the orifice temperature is known. The orifice temperature was assumed to be 60 $^{\circ}\text{F}$ for the preliminary run and then determined from that run.

FACILITY: _____ DATE: _____
 LOCATION: At GLE N. 1/4 Sec. 10, T. 10 N., R. 10 E., S. 10 E. TIME: 12:30 PM
 CONTACT: _____ J. A. LARSON. POSITION: Plant Manager
 AMBIENT TEMPERATURE: 50 °F WEATHER: Clear
 BAROMETRIC PRESSURE: 22.24 "Hg
 PLANT PRODUCTION: 85 tons/hr. TONS PER _____ HOURS

middle stack	Run No.	Filter No.	Sample Time minutes	ΔH inches H ₂ O	Orifice Temperature °F
	1	13	2.0	.46	75
	2	14	2.0	.46	75
	3	15	2.0	.46	75
	4	16	2.0	.46	75
	5	17	2.0	.46	75
	6	18	2.0	.46	75
south stack	1	19	2.0	.46	75
	2	20	2.0	.46	75
	3	21	2.0	.46	75
	4	22	2.0	.46	75
	5	23	2.0	.46	75
	6	24	2.0	.46	75

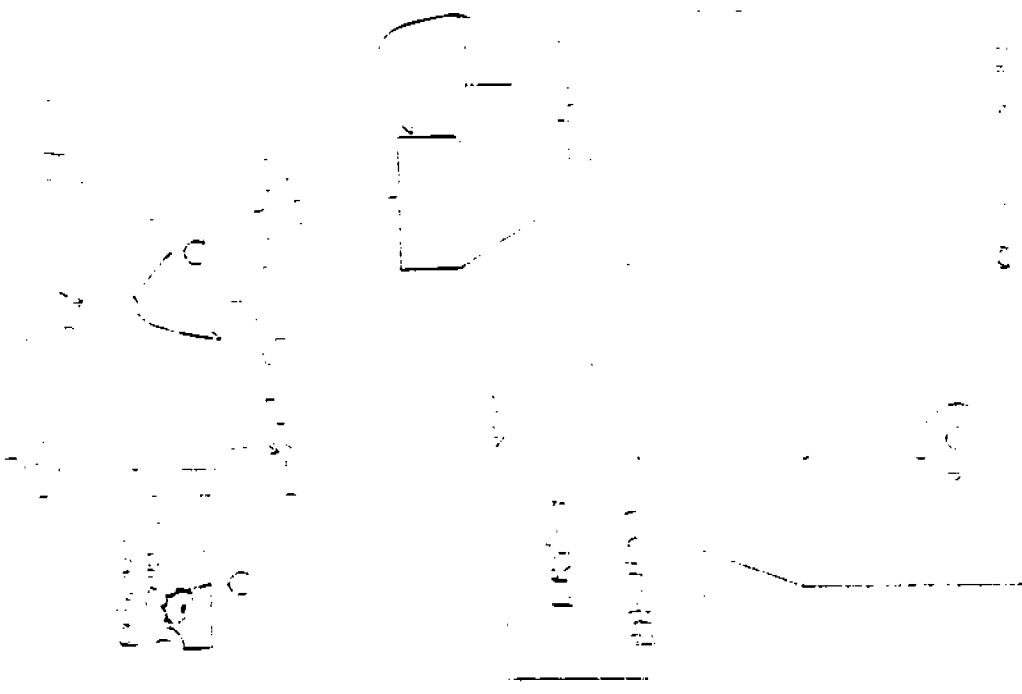
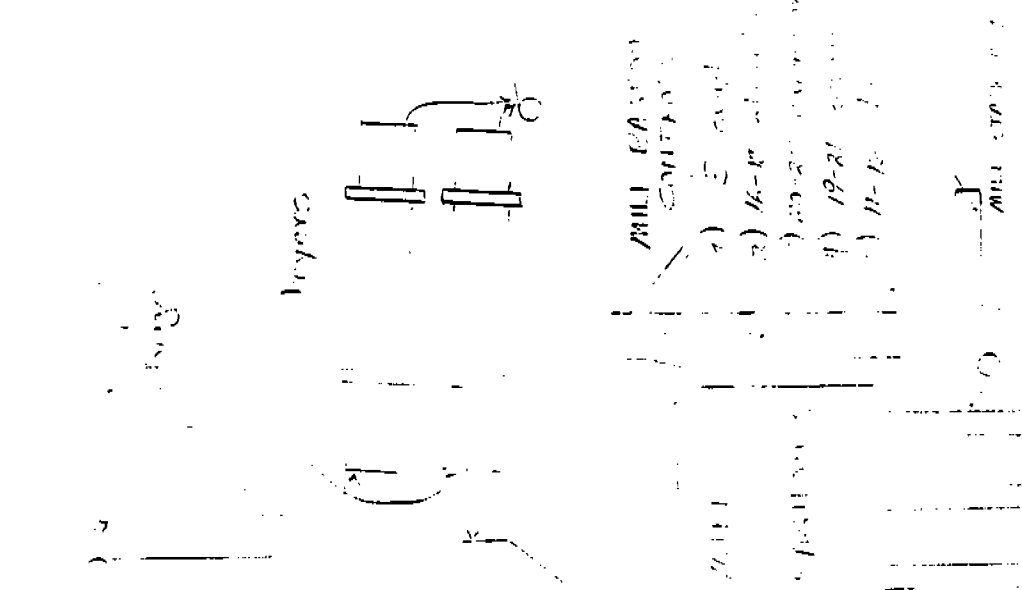
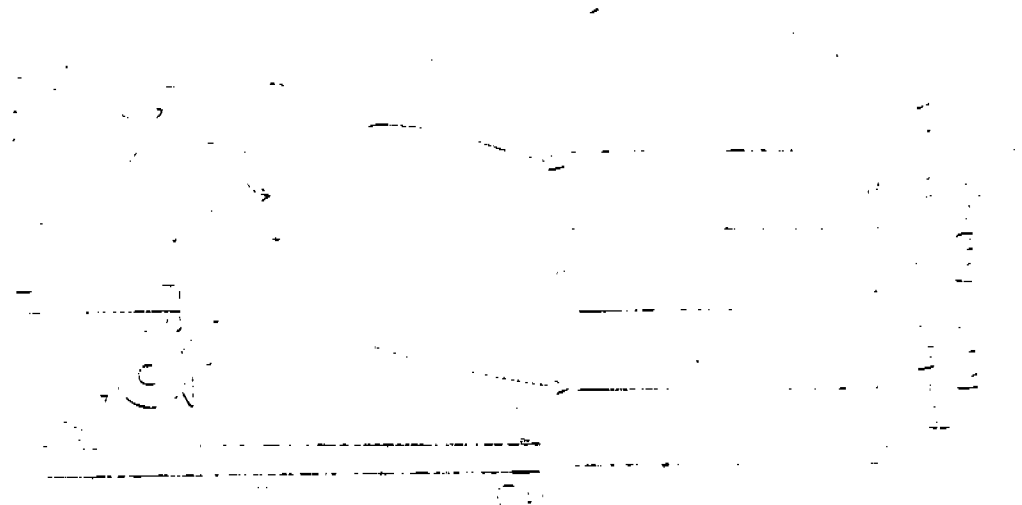
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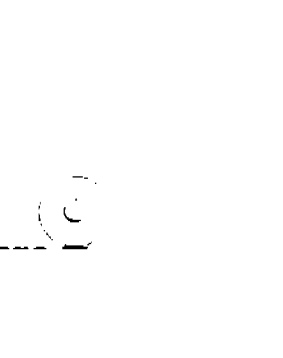
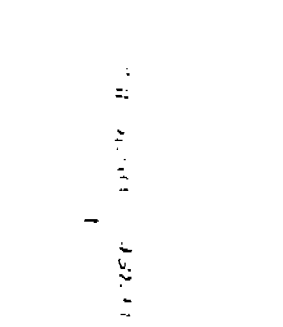
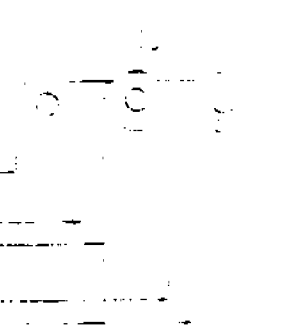
NOTES:

T _o	ΔH

JOHNS- MANVILLE

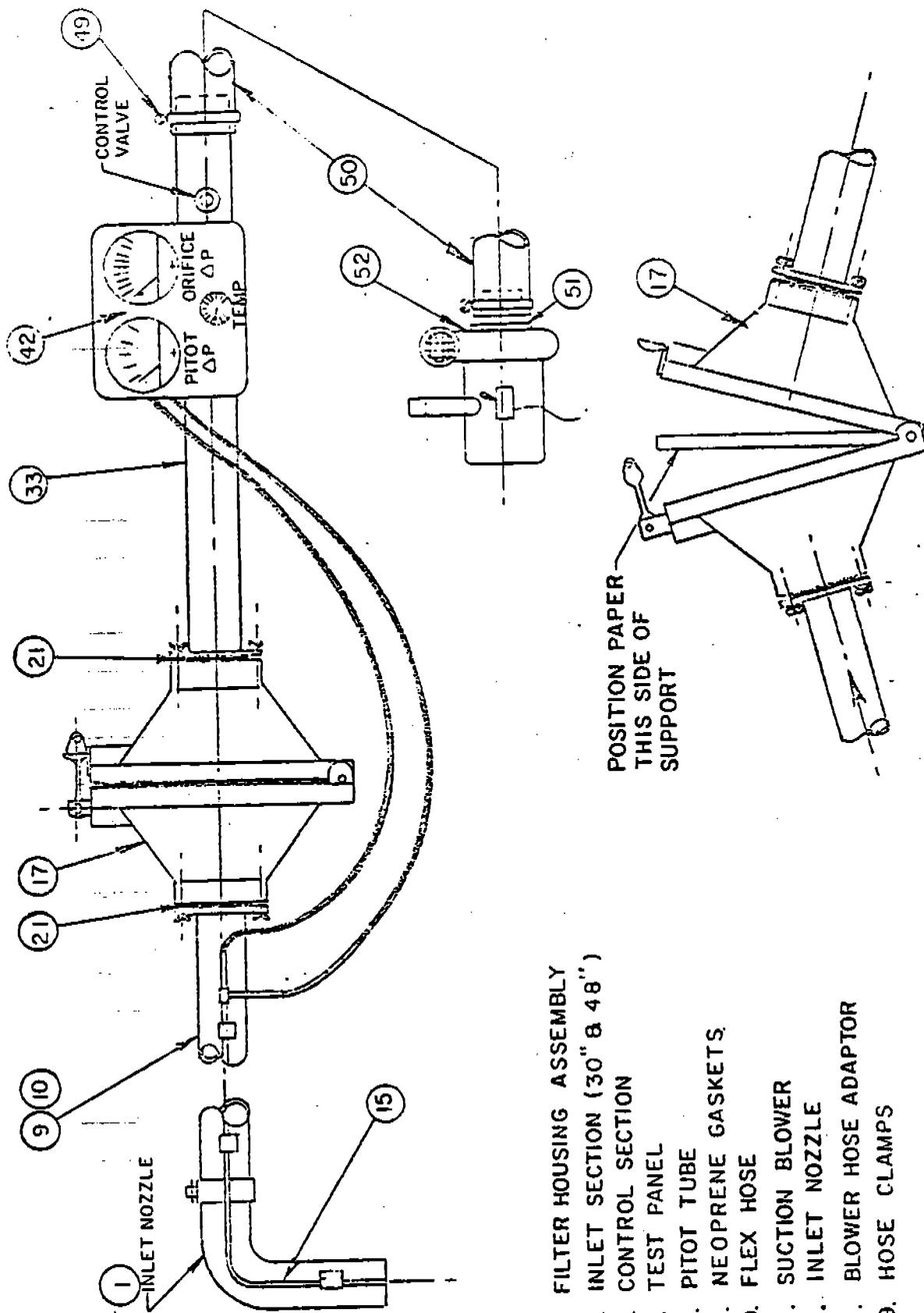


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- 100) 1/2" NPT



used at
Mill Baghouse

Must Measure Change



- 17. FILTER HOUSING ASSEMBLY
- 9410. INLET SECTION (30" & 48")
- 33. CONTROL SECTION
- 42. TEST PANEL
- 15. PITOT TUBE
- 21. NEOPRENE GASKETS
- 50. FLEX HOSE
- 52. SUCTION BLOWER
- 1. INLET NOZZLE
- 51. BLOWER HOSE ADAPTOR
- 49. HOSE CLAMPS

REV. 10-67



RADER PNEUMATICS

TITLE RADER HI-VOLUME SAMPLER

SCALE

DATE 7-30-71

DRWN. J.W. HIRSCH
CKD.

A-100332A

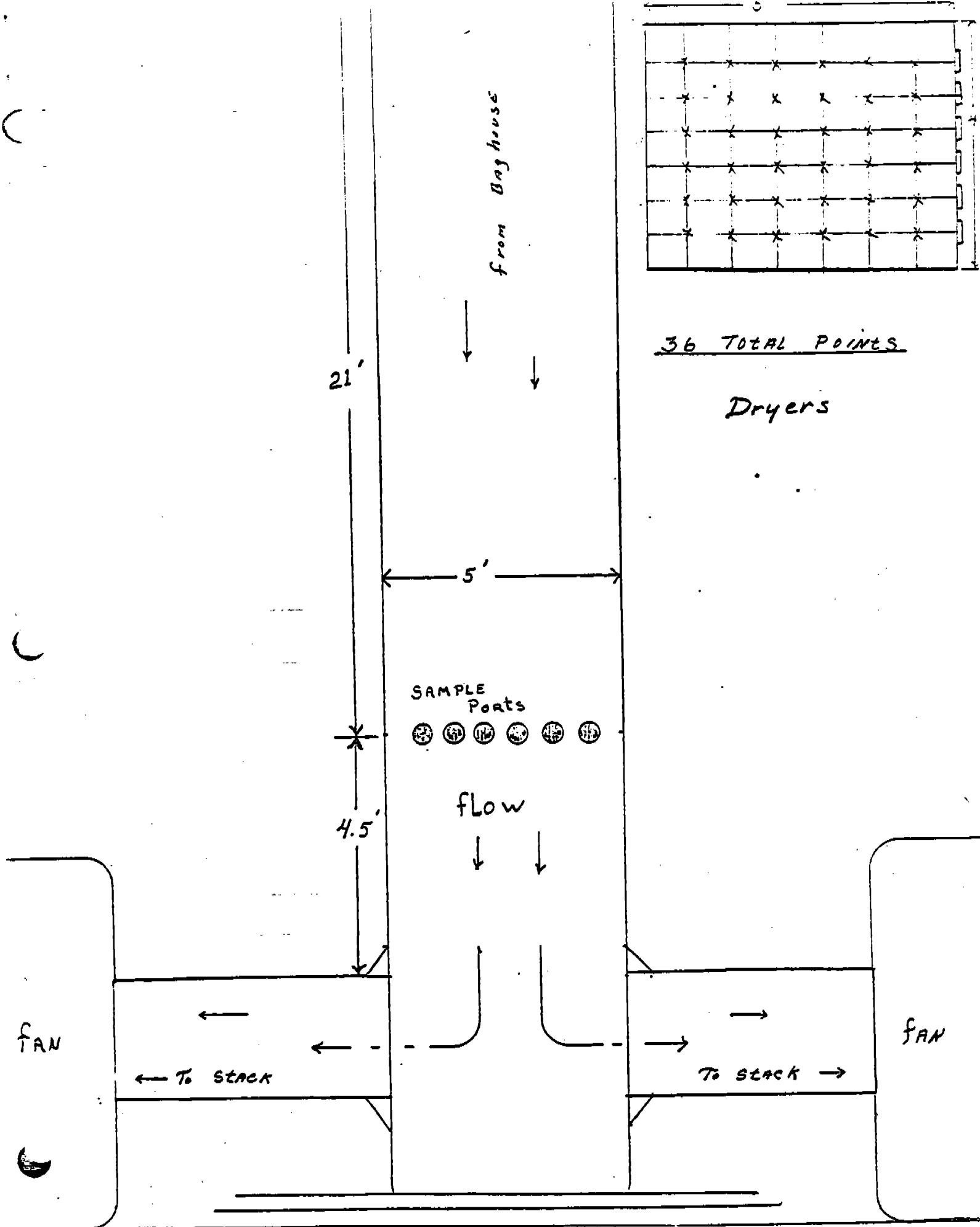
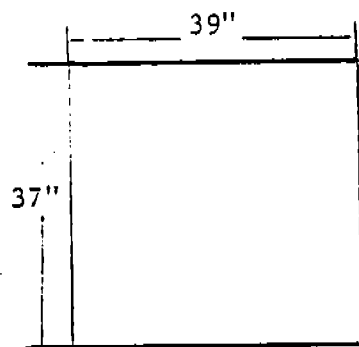
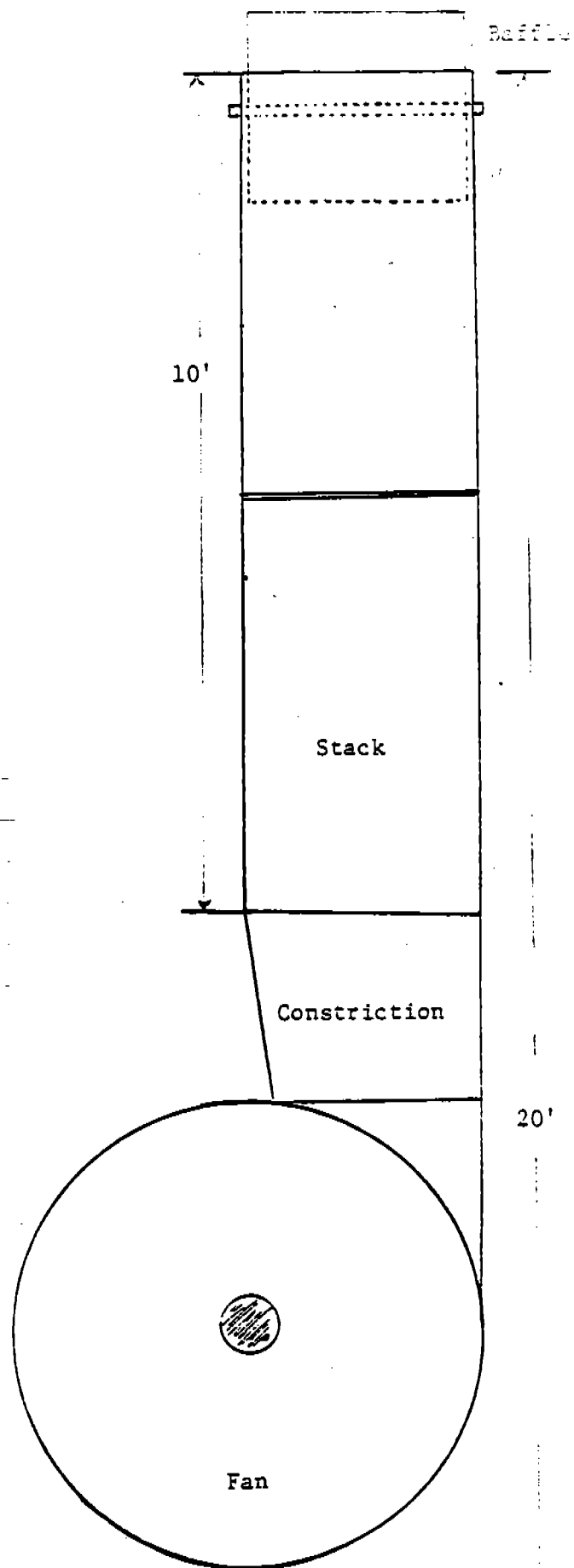


Figure 2



Cross Section Stack



One of four stacks from the mill baghouse.

Figure 1

Temperature
Sensor

Check
Valve

Vacuum
Line

Temperature
Sensor

Filter Holder

Pitot Tube Gauge

Temperature
Sensor

S-Type
Pitot Tube

Stack Wall

Cyclon

Heated
Area

Flask

Standard
Impinger

Modified Impingers

By-Pass
Valve

Vacuum
Gauge

Main
Valve

Pump

Temperature
Sensor

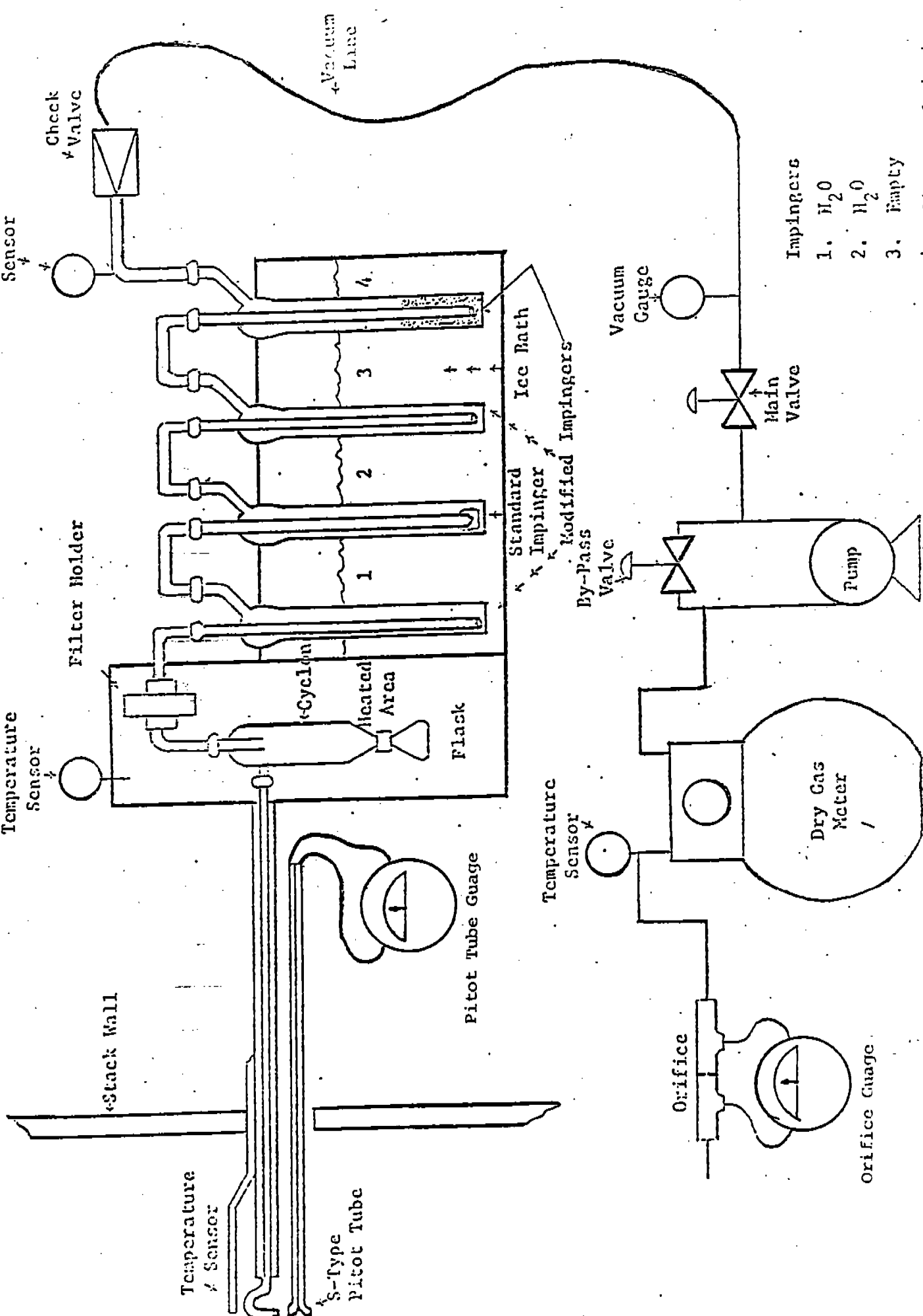
Dry Gas
Meter

Orifice

Orifice Gauge

Impingers

1. H_2O
2. H_2O
3. Empty
4. Empty



Plant: Donner 110
 Date: 2/12/21
 Location: NO. 1000 New Mexico
 Operators: J. Romero, T. Barker, M. P. Jones
 Stack No.: Dryer Port Identifi: 3.00 ft.
 Fan No. or Test: II
 Type of Test: Total Particulate
 Stack Diameter, in.: 48" x 1.0"
 Meter Box No.: IV
 Probe No.: 110
 Ambient Temperature: 76
 Barometric Pressure: 27.07
 Static Pressure:
 Pitot Tube Coeff.: .83
 Probe Length, in.: 72"
 Process Weight Rate: 55 T/H
 Time Test Started: 5:40 P.M.
 Time Test Ended: 7:00 P.M.
 Plant Arrival: 3:00 P.M.
 Plant Contact: Dave Land

1. Meter RH: 14.2
 2. Moisture %: 18.0%
 3. Meter Temperature: 95
 4. Ps/Pm:
 5. Temperature of Stack:
 6. Average IP:
 7. Actual Nozzle Diameter: .255
 8. Average AH:

Traverse Point Number	Sampling Time in Min.	Velocity Head (FPS) (MPS)	Pressure Differential Across Orifice Meter (in. H ₂ O)	Gas Sample Volume (ml) (ft. ³)	Stack Temperature (°F) (°C)	Temperature Probe (°F) (°C)	Temperature Box (°F) (°C)	Temperature Impinger Out (°F) (°C)	Temperature In (°F) (°C)	Temperature Meter Out (°F) (°C)	Pump Vacuum in Hg gauge
1	2	12 346	.27	7142.13	180	230	240	60	175	70	5.5
2	4	12 346	.27		180	230	240	55	175	70	5.5
3	6	42 .648	.94	7144.6	180	240	250	60	175	70	7.0
4	8	39 .624	.88		180	240	250	60	175	75	7.0
5	10	40 .632	.90	7147.0	180	240	250	55	180	75	8.0
6	12	44 .663	1.0	7149.43	180	230	250	55	180	75	9.0
1	2	14 800	.45	7148.43	180	220	240	60	160	75	11.0
2	4	50 .707	1.12		180	260	210	55	170	75	8.5
3	6	50 .707	1.12	7151.6	180	200	210	55	170	75	8.5
4	8	40 .632	.90		180	250	250	60	190	75	7.5
5	10	40 .632	.90	7154.7	180	250	260	60	200	75	7.5
6	12	30 .616	.80		180	250	280	65	215	80	7.0
1	2	55 742	1.52	7157.7	180	250	300	65	175	80	9.0
2	4	54 735	1.2		180	250	300	65	175	80	9.0
3	6	44 .663	1.0	7160	180	250	300	60	225	85	8.0
4	8	52 .698	.94		180	250	300	60	230	85	7.5
5	10	44 .663	1.0	7163.5	180	250	300	60	230	85	7.5
6	12	53 725	1.2	7166.0	180	250	300	60	250	85	9.0
1	2	53 725	1.2		180	250	300	60	250	85	9.0

WEIRAGE	IMPINGER VOLUME (ml)	SILICA GEL WEIGHT (g)
VOLUME OF LIQUID WATER COLLECTED	1 2 3 4	
FINAL	208409 1	679
INITIAL	100400 0	659
NO COLLECTED	108 5 1	15
TOTAL VOLUME COLLECTED		

TYPE OF ORIFICE MEASUREMENT	TIME	CO ₂	O ₂	CO	N ₂
1	1.0	200			
2	1.0	240			
3	1.0	260			

Initial Leak Check:
 Final Leak Check:

High pressure H₂O used, a 0.150" H₂O changed initial and final after second point.

I

Traverse Point Number	Sampling Time in Min.	Velocity Head (FPS) ($\sqrt{FPS}$)	Pressure Differential Across Orifice Meter (IN) "H ₂ O"	Gas Sample Volume (Nm) ft. ³	Stack Temperature (Ts) °F	Temperature Probe °F	Box °F	Temperature Impinger Out °F	In °F	Temperature Water Out °F	Pump Vacuum in Hg gauge
1	2	33 574	79.74	7164.0	180	260	300	65	220	85	6.5
2	4	36 510	79		180	260	300	65	225	85	6.0
3	6	34 583	76	7168.5	180	260	300	65	230	85	6.5
4	8	42 648	94		180	260	300	60	240	90	7.5
5	10	38 616	86	7171.5	180	260	300	60	240	90	7.0
6	12	42 648	94	7173.75	180	260	300	60	240	95	7.5
1	2	.50 .707	1.12	7173.75	180	260	300	70	240	100	7.8
2	4	.41 663	.99		180	260	300	70	245	100	7.5
3	6	.40 632	.90	7179.0	180	260	300	60	245	100	7.0
4	8	.38 616	.86		180	260	300	60	245	100	7.0
5	10	.42 648	.94	7179.5	180	260	300	55	245	100	7.5
6	12	.40 632	.90	7182.24	180	260	300	55	245	100	7.0
1	2	.58 .767	1.30	7182.24	180	260	300	55	245	105	8.5
2	4	.48 693	1.07		180	260	300	55	245	105	8.0
3	6	.42 648	.94	7185.3	180	260	300	55	245	105	7.0
4	8	.38 616	.86		180	260	300	55	245	105	7.0
5	10	.34 583	.76	7185	180	260	300	55	245	105	6.0
6	12	.28 529	.63		180	255	290	50	245	105	5.5

103

Final 7190.59

48.46 C.F.

Pressure Drops Baghouse ("H₂O)

#1 #2 #3 #4 -5 Phosphate

5.5 5.4 5.3 5.7 5.9 5.7

Plenum

2.4"

1. Ambient Temperature: 52.0
 2. Barometric Pressure: 29.92
 3. Static Pressure: -14.5
 4. Pitot Tube Coeff: 0.9
 5. Probe Length, in.: 72"
 6. Process Weight Rate: 45 Tons/hr
 7. Time Test Started: 5:10 PM
 8. Time Test Ended: _____
 9. Plant Arrival: 5:25 PM
 10. Plant Contact: DR. LAIRD

1. Meter LHS: _____
 2. Moisture %: _____
 3. Meter Temperature: _____
 4. Ps/Pm: _____
 5. Temperature of Stack: _____
 6. Average ΔP : _____
 7. Actual Nozzle Diameter: 2.5"
 8. Average ΔH : _____

Points: _____
 Date: 5/27
 Location: 4000 - 1000
 Operators: W. B. & R. B.
 Stack No.: 7000 Port Identif: 7000
 Run No. or Test: 1
 Type of Test: Test - 1000
 Stack Diameter, in.: 48"
 Meter Box No.: 100
 Probe No.: 116

[illegible]

VOLUME OF LIQUID WATER COLLECTED	EXPANDER VOLUME (ml)				SILICA GEL WEIGHT (g)
	1	2	3	4	
FINAL	202	115	4		669
INITIAL	100	100	0	-	654
TO BE COLLECTED	102	15	4		10
TOTAL VOLUME COLLECTED	131				

Initial Leak Check: _____
Final Leak Check: _____

WATER COLLECTED	WEIGHT (g)				PYRITE OR ORSP. MEASUREMENT	TIME	CO ₂	O ₂	CO	N ₂
	1	2	3	4						
FINAL	202	115	4	-	66A	1	5.00	2.0	190	
INITIAL	100	100	0	-	65A	2		2.0	190	
RE-WEIGHTED	102	115	1	-	66	3		2.0	190	

SECRET

Personnel	Change	Number	Change	Percentage	'13
1	12	1	12	100	
2	6	7	6	85	
3	6	7	6	85	

TEST NUMBER

DATE:

2/10/51

Traverse Point Number	Sampling Time in Min.	Velocity Head (fps) (fps)		Pressure Differential Across Orifice Meter (in) H ₂ O	Gas Sample Volume (in) ft. ³	Stack Temperature (T _s) °F	Temperature Probe °F		Temperature Impinger Out °F In °F		Temperature Water Out °F	Pump Vacuum in Hg gauge
	5	34	.583	.82	7217.19	180	270	270	65	210	100	7.5
	10	37	.616	.92		180	270	270	65	210	100	8.0
3	5	40	.632	.98	7220.0	180	270	280	65	230	105	8.5
4	5	40	.632	.98		180	270	280	65	235	105	8.5
5	10	42	.648	1.02	7222.5	180	270	280	60	235	105	8.5
6	12	40	.632	.98	7225.43	180	270	280	60	235	105	8.5
1	2	50	.707	1.2	7225.43	180	270	290	65	225	105	10.5
2	4	30	.548	.72		180	270	290	65	225	105	7.0
3	6	20	.447	.48	7228.4	180	270	290	60	240	110	5.0
4	8	16	.400	.39		180	270	290	60	245	110	4.5
5	10	16	.400	.39	7230.0	180	270	290	60	245	110	4.5
6	12	19	.436	.46	7232.0	180	270	290	60	245	110	5.0
1	2	45	.671	1.1	7232.06	180	270	300	70	225	115	9.5
2	4	40	.632	.98		180	270	300	70	225	115	9.0
3	6	44	.663	1.07	7235.3	180	270	300	70	225	115	9.0
4	8	36	.600	.88		180	270	290	60	240	115	8.0
5	10	40	.632	.98	7237.8	180	270	290	60	245	115	8.5
6	12	42	.648	1.02		180	270	290	60	230	115	9.0

Total Reading 7240.70

PARTICULATE FIELD DATA

Date: 2/1/81 Ambient Temperature: 52 Meter ΔH : 1.47
 Location: Port Arthur, Texas Barometric Pressure: 22.25 Moisture %:
 Operators: A. P. Jones, T. Carter, M. R. Jones Static Pressure: -8.2 Meter Temperature: 25
 Stack No.: Drivers Port Identification: Pitot Tube Coeff: 83 Ps/Pm: .97
 Run No. or Test: IR Probe Length, in.: 7.2 Temperature of Stack: 180
 Type of Test: Total Particulate Process Weight Rate: 80 Tons/hr Average ΔP : 1.58
 Stack Diameter, in.: 48" x 60" Time Test Started: 5:00 P.M. Actual Nozzle Diameter: .250
 Meter Box No.: Time Test Ended: 7:20 P.M. Average ΔH : 1.765
 Probe No.: 110 Plant Arrival: 2:00 P.M. Plant Contact: DAVID LAIRD

Traverse Point Number	Sampling Time in Min.	Velocity Head (APs) (IPs)	Pressure Differential Across Orifice Meter (in) "H ₂ O"	Gas Sample Volume (V _m) ft. ³	Stack Temperature (T _s) °F	Temperature Probe °F	Box °F	Temperature Impinger Out °F	In °F	Temperature Meter Out °F	Pump Vacuum in Hg gauge	
1	2	52	221	1.15	7241.05	180	280	280	70	125	80	11.5
2	4	52	221	1.15		180	280	280	70	155	80	11.5
3	6	52	721	1.15	7246.00	180	290	300	70	160	80	11.5
4	8	50	707	1.1		180	290	300	60	190	85	11.5
5	10	50	707	1.1	7247.0	180	290	300	60	190	85	11.5
6	12	50	707	1.1	7250.0	180	290	300	60	190	85	11.5
					10							
1	2	46	678	1.08	7250.0	180	270	290	65	180	85	10.5
2	4	44	663	.98		180	270	290	60	180	85	10.5
3	6	44	663	.98	7253.0	180	270	290	60	180	85	10.5
4	8	44	663	.98		180	270	290	60	215	85	10.5
5	10	48	693	1.07	7255.7	180	270	290	60	220	90	11.0
6	12	48	693	1.07	7258.65	180	270	290	60	220	90	11.0
1	2	34	583	.76	7258.65	180	270	290	65	190	95	8.5
2	4	24	490	.53		180	270	300	65	220	95	7.5
3	6	24	529	.62	7261.0	180	270	300	65	225	95	7.5
4	8	32	506	.71		180	270	300	65	225	95	8.0
5	10	34	583	.78	7263.7	180	275	300	65	235	95	8.5
6	12	36	600	.80	7266.0	180	275	300	65	235	95	8.5

TOTAL

AVERAGE

VOLUME OF LIQUID WATER COLLECTED	IMPINGER VOLUME (ml)				SILICA GEL WEIGHT (g)
	1	2	3	4	
FINAL	202	114	3	-	269
INITIAL	100	100	0	-	200
WATER COLLECTED	102	14	3		
TOTAL VOLUME COLLECTED					

TYPE OR GROSS MEASUREMENT	TIME	CO ₂	O ₂	CO	N ₂
1		20	180		
2		20	180		
3		20	180		

Don't Stop @ 17" min Initial Leak Check: 1.14

Final Leak Check: Don't Stop @ 12" min

Pressure drop across pump length = 1.1
 = 2.3 4.9 6.5 16.1

2 5.0 5.0 4.0 4.7 4.5 2.8

02/18/71

Traverse Point Number	Sampling Time in Min.	Velocity Head (FPS) (FPS)	Pressure Differential Across Orifice Meter (IN) "H ₂ O"	Gas Sample Volume (L) (L)	Stack Temperature (TS) °F	Temperature Probe °F	Temperature Box °F	Temperature Impinger Out °F	Temperature Impinger In °F	Temperature Meter Out °F	Pump Vacuum in Hg Gauge
1	2	36.600	90	7246.0	180	280	310	65	265	100	8.5
2	4	29.529	62		180	280	310	65	210	100	7.0
3	6	31.557	68	7268.8	180	285	310	65	240	100	7.5
4	8	29.530	64		180	285	310	65	245	100	7.5
5	10	29.539	64	7270.8	180	285	310	65	250	100	7.5
6	12	32.566	71	7273.5	180	285	310	65	250	100	8.0
1	2	26.510	58	7273.5	180	285	310	65	220	100	6.5
2	4	20.447	44		180	280	320	70	245	105	5.5
3	6	22.469	48	7276.5	180	280	320	70	245	105	5.5
4	8	26.510	58		180	280	320	70	245	105	6.5
5	10	28.529	62	7278.6	180	280	320	65	250	105	6.5
6	12	32.566	71	7278.8	180	280	320	65	250	10.5	7.5
1	2	44.663	98	7279.8	180	280	320	70	235	110	9.0
2	4	14.374	31		180	280	320	65	250	110	4.0
3	6	22.469	48	7282.4	180	280	315	65	250	110	5.5
4	8	18.424	40		180	280	315	65	250	110	4.5
5	10	20.447	44	7284.0	180	280	295	65	240	110	5.5
6	12	22.469	48		180	280	290	65	240	110	5.5

58 Final Reading 7286.11
769

96

Pressure drops across 1200 house (Last Port)

#1	#2	#3	#4	#5	#6	Plenum
5.5"	5.3	5.3	5.8	5.8	5.7	2.8

CALCULATED EMISSIONS

MILL

Table 2.

Run No.	Time minutes	Filter No.	Particulate Weight, gm		Vm cf	Wt. lb./hr.
			Net	Adjusted		
1	2.0	1	.0527	.0554	69.7	3.535
2	2.0	2	.0385	.0412	69.7	2.629
3	2.0	3	.0273	.0300	69.7	1.914
4	2.0	4	.0435	.0462	69.7	2.948
5	2.0	5	.0215	.0242	69.7	1.544
6	2.0	6	.0263	.0290	69.7	1.850
7	2.0	7	.0418	.0445	69.7	2.840
8	2.0	8	.0387	.0414	69.7	2.642
9	2.0	9	.0531	.0558	69.7	3.561
10	2.0	10	.0305	.0332	69.7	2.118
11	2.0	11	.0276	.0303	69.7	1.933
12	2.0	12	.0417	.0444	69.7	2.833
13	2.0	13	.0222	.0249	69.7	1.589
14	2.0	14	.0201	.0228	69.7	1.455
15	2.0	15	.0339	.0366	69.7	2.335

Tare Weight Changes

Filter No.	Wt. Change gm
26	.0009
27	.0017
Average	.0013

Average: 1.764 lb./hr.

Standard Deviation: 9102 lb./hr.

Total Sampling Time: 48 minutes

Probe Washing Weight: 99.4 grams

" " Blank - 4.2
95.2 grams

CALCULATED EMISSIONS

MILL

Table 2.

Run No.	Time minutes	Filter No.	Particulate Weight, gm		Vm cf	Wt. lb./hr.
			Net	Adjusted		
16	2.0	16	.0119	.0146	69.7	.9316
17	2.0	17	.0114	.0191	69.7	.8997
18	2.0	18	.0269	.0296	69.7	1.8888
19	2.0	19	.0063	.0090	69.7	.574
20	2.0	20	.0044	.0071	69.7	.453
21	2.0	21	.0043	.0070	69.7	.417
22	2.0	22	.0055	.0082	69.7	.523
23	2.0	23	.0046	.0073	69.7	.466
24	2.0	24	.0041	.0068	69.7	.434

Tare Weight Changes

Filter No.	Wt. Change gm
26	.0009
27	.0017
Average	.0013

Average: 1.764 lb./hr.

Standard Deviation: 9102 lb./hr.

Total Sampling Time: 48 minutes

Probe Washing Weight: .0994 grams

Probe washing Blank - 4.2 grams

.0052 grams

DATE RECEIVED 2-23-71

LABORATORY NUMBER AF-3308-33

CHEMICAL ANALYSES OF STATIONARY SOURCE EMISSIONS IN AIR

COLLECTION DATE 2/16/71 10:00 - 10:15

SOURCE Iron Mine - P. O. Box 968

COLLECTED BY A. Romero, F. Romero, L. Romero

SOURCE LOCATION NE 12th St. N. 17th St.

REPORT TO Jimmy Romero, Env. Scientist III

OTHER INFORMATION

ADDRESS E.I.D. - Air Quality Bureau

P. O. Box 968 - Crown Bldg.
 Santa Fe, NM 87503

Dryer Baghouse

SAMPLE DESCRIPTION AND NUMBER	SAMPLE VOLUME (ml)	TOTAL PARTIC- ULATE (mg)	OXIDES OF NITROGEN (μg)	SULFUR DIOXIDE		OTHER ANALYSES	NOTES
				VOLUME TITRATED V _a (ml)	VOLUME TITRANT V _t (ml)		
<u>AF-3308</u>	<u>130.</u>	<u>15.4</u>	☐	☐	☐	☐	
<u>AF-3309</u>	<u>147.</u>	<u>50.9</u>	☐	☐	☐	☐	
<u>AF-3310</u>	<u>196.</u>	<u>30.7</u>	☐	☐	☐	☐	
<u>AF-3311</u>	<u>140.</u>	<u>22.7</u>	☐	☐	☐	☐	
<u>AF-3312</u>	<u>328.</u>	<u>2.5</u>	☐	☐	☐	☐	
<u>AF-3313</u>	<u>164.</u>	<u>99.4</u>	☐	☐	☐	☐	
<u>AF-3314</u>	<u>316.</u>	<u>4.2</u>	☐	☐	☐	☐	

DATE ANALYSED 2-23-71

ANALYST AF-3314

FILTER WEIGHT RECORD

Facility St. Louis, Mo. Testing Dates 5/16-17-18-19/61

Date of Tare Weighing 2-13-51 Weighed By [Signature]

Date of Final Weighing 3-6-81 Weighed By Tom Baker

Type of Test: ☒ EPA Particulate

ASME Alundum Thimble

 Rader

	Other
---	-------

Type of Filter 110 cm Glass Fiber

Dryer Baghouse

[illegible]

Test
Not Calculator

FILTER WEIGHT RECORD

Facility John Deere Testing Dates 2-18-81

Date of Tare Weighing 2-13-81 Weighed By Tom Beck

Date of Final Weighing 3-6-81 Weighed By Tom Beck

Type of Test: ☐ EPA Particulate

☐ ASME Aluminum Thimble

☒ Rader

☐ Other _____

Type of Filter Type A Glass Fiber 8x10 inch
Mill Baghouse

Filter No.	Tare Weight mg	Final Weight mg	Particulate Weight grams
1	3.6955	3.7462	0.0527
2	3.4366	3.4691	0.0325
3	3.4322	3.4595	0.0273
4	3.7113	3.7548	0.0435
5	3.4182	3.4397	0.0215
6	3.4881	3.4364	0.0263
7	3.4493	3.4911	0.0418
8	3.7014	3.7401	0.0387
9	3.4472	3.4963	0.053
10	3.4034	3.4339	0.0305
11	3.4552	3.4319	0.0271
12	3.7140	3.7557	0.0417
13	3.4412	3.4412	0.0000
14	3.7170	3.7377	0.0207
15	3.4252	3.4592	0.0339

FILTER WEIGHT RECORD

Facility State Mills Testing Dates 3-18-51
 Date of Tare Weighing 2-12-51 Weighed By Tom Rader
 Date of Final Weighing 3-6-51 Weighed By Tom Rader

Type of Test: ☐ EPA Particulate
☐ ASME Alundum Thimble
☒ Rader
☐ Other _____

Type of Filter Type A Glass Fiber 8x10 inch

Mill Baghouse

Filter No.	Tare Weight grams	Final Weight grams	Particulate Weight grams
16	3 7046	3 7165	0.0119
17	3 7138	3 7252	0.0114
18	3 3953	3 4222	0.0269
19	3 4243	3 4306	0.0063
20	3 7296	3 7346	0.0050
21	3 5322	3 5375	0.0053
22	3 5640	3 5695	0.0055
23	3 6251	3 6797	0.0546
24	3 5757	3 5838	0.0081
25	1 5 0		
26	3 5 7	3 5403	0.0009
27	3 6478	3 6495	0.0017

N.M. Environmental Improvement Agency

ENVIRONMENTAL SAMPLE TRANSMITTAL

TO: (Name & Address)

FROM: (Name & Address)

Sample Location:

Field Sample
Number

Preservative

Analysis Required

Lab Number

Test #1

Acetone

Total Particulates

Hy-3308

Test #2

"

"

Hy-3309

Test #3

"

"

Hy-3310

Test #4

"

"

Hy-3311

Blank Test

"

"

Hy-3312

Dryer

"

"

Hy-3313

Blank

"

"

Hy-3314

Blank

"

"

To Be Completed By Field Personnel

Prepared By:

(signature)

Date:

Time:

Field Notebook Number:

Method of Shipment:

To Be Completed By Receiving Laboratory

Received By:

(signature)

Date:

Time:

Originating Office: Prepare in quadruplicate. The original and one copy will accompany sample shipment. Mail one copy directly to the addressee and one copy will be retained by the Survey Coordinator for reference.

Receiving Office: After receiving samples, assign Lab Number and return the original to the Survey Coordinator. Retain one copy for laboratory files.

CALIBRATIONS

Johns-Manville February 16, 17, 18 and 19, 1981

<u>EPA Box</u>	<u>MCF</u>	<u>ΔH@</u>	<u>Date</u>	<u>By</u>
I	1.02	1.53	2/10/81	M. Romero
IV	.99	1.47	10/17/80	M. Romero

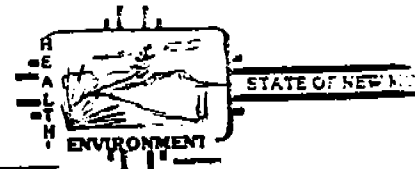
<u>Probe</u>	<u>T.S. dev.</u>	<u>Date</u>	<u>By</u>
110	- 0.09	8/27/80	T. Booker
107	no recent data		

<u>EPA Box</u>	<u>M.O. dev.</u>	<u>Date</u>	<u>By</u>
I	1.4	11/18/80	T. Booker
IV	0	8/28/80	T. Booker

<u>Pitot Tube</u>	<u>Cp</u>	<u>Cp w/nozzle</u>	<u>Date</u>	<u>By</u>
110	.83	.83	2/12/81	M. Romero
102	.83	.81	5/16/80	M. Romero

<u>Probe Tip</u>	<u>Size</u>	<u>Actual Size</u>	<u>Date</u>	<u>By</u>
A	1/4	.255	2/17/81	J. Romero
B	1/4	.250	2/19/81	J. Romero

ENVIRONMENTAL IMPROVEMENT DIVISION RECORD OF VISUAL DETERMINATION OF OPACITY



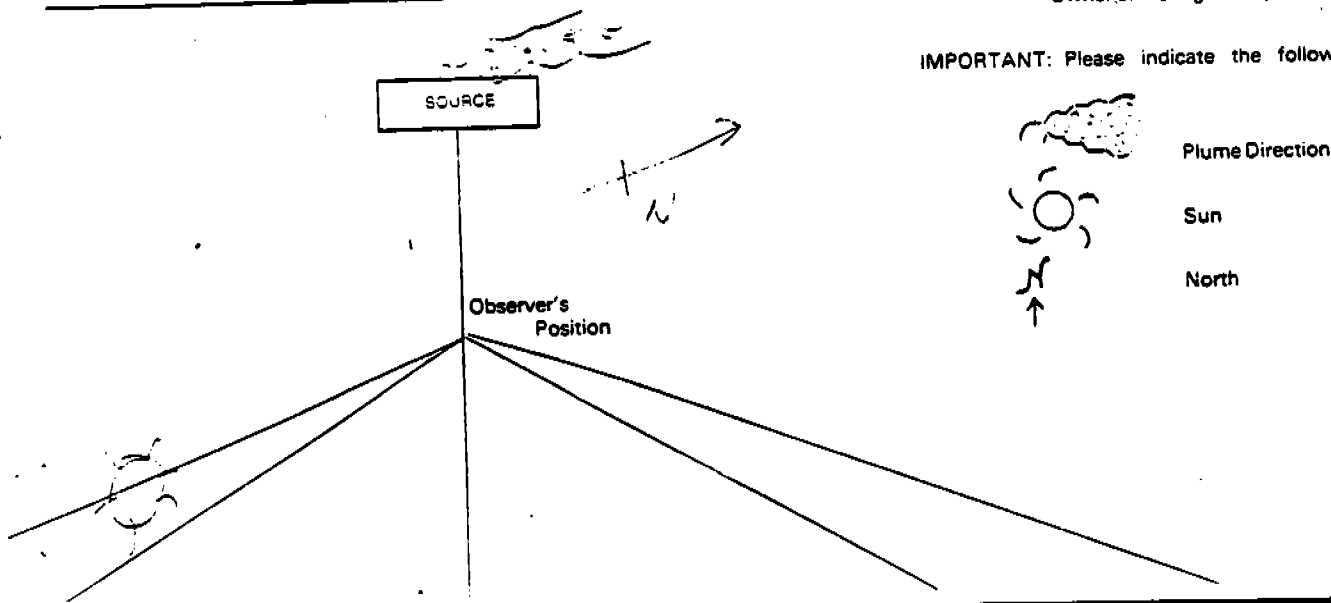
Company Tahm-Moon Ho Perlite
 Location Al. Agua Observer Steve Schnabelke
 Test Number 4 Observer Certification Date 10-22-80
 Date 2-17-81 Observer Affiliation NM EID Air Quality
 Type of Facility perlite plant Point of Emission top of stack #1
 Control Device baghouse Height of Discharge Point 30

	Initial	Final	Record Opacity in % 5% Smallest Division					OPACITY AVERAGE	
			sec min	0	15	30	45	Sum of No. Recorded	
Clock Time	12:40	12:51:15	1	5	0	0	5	100	
Observer Location	75'	"	2	0	0	5	5		
Distance to Discharge	east	"	3	0	0	0	0	40	
Direction from Discharge	55'	"	4	0	0	0	0		
Height of Observation Pt.	east red	"	5	0	0	0	0	Average Opacity	
Background Description	SE → NW	"	6	0	5	0	0		
Weather Conditions	0-10	"	7	5	10	10	5	2.5	
Wind Direction	55°F	"	8	5	0	5	0		
Wind Speed	clear	"	9	10	10	5	0	Opacity Range	
Ambient Temperature	white	"	10	5	0	5	0		
Sky Condition (clear, over-cast, % clouds, etc.)	5' max	"						0 % to 10 %	
Plume Description									
Color									
Distance Visible									
Other Information									
Comments:									

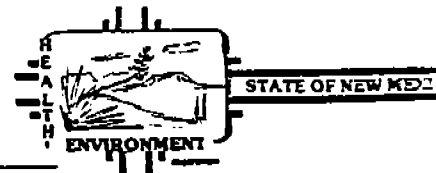
Steve Schnabelke
Observer's Signature

Owner or Manager of Operation

IMPORTANT: Please indicate the following by sketch:



ENVIRONMENTAL IMPROVEMENT DIVISION
RECORD OF VISUAL DETERMINATION OF OPACITY



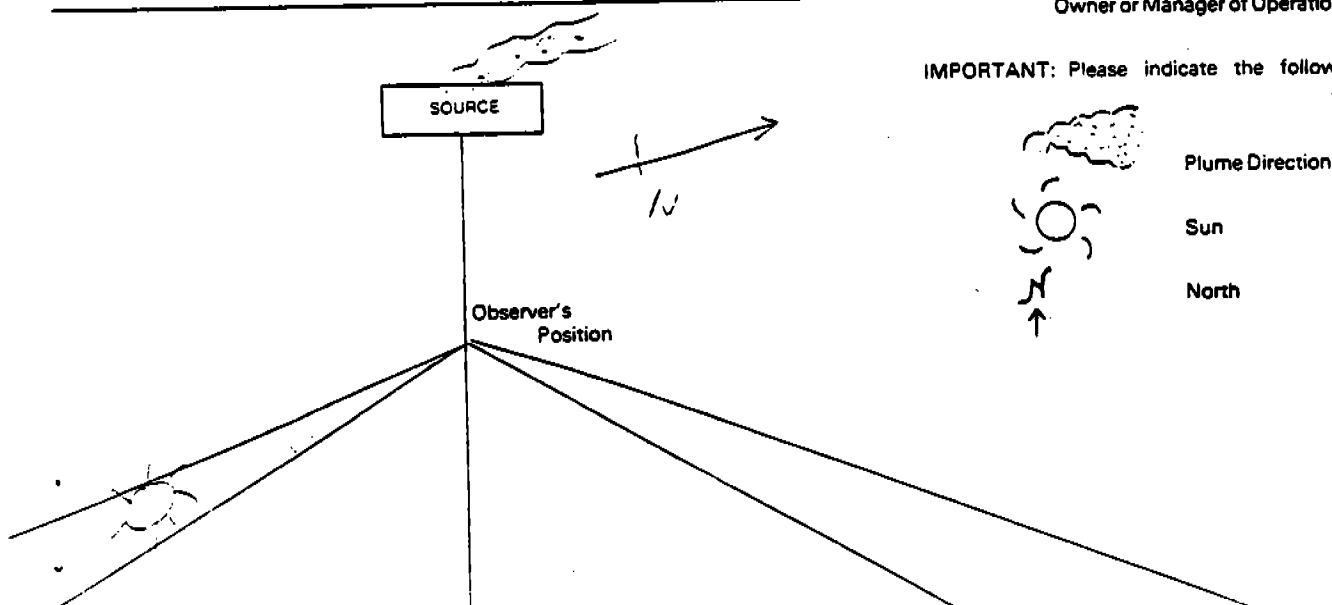
Company Tolson - Manville Facility
Location La Pava Observer Steve Schuebke
Test Number 3 Observer Certification Date 10-22-80
Date 2-17 Observer Affiliation NM EID Air Quality
Type of Facility baghouse Point of Emission top of stack #2
Control Device baghouse Height of Discharge Point 30'

	Initial	Final	Record Opacity in % 5% Smallest Division				OPACITY AVERAGE	
			sec min	0	15	30		45
Clock Time	12:22	12:32:45					Sum of No. Recorded	
Observer Location								
Distance to Discharge	75'	"	1	0	0	0	5	90
Direction from Discharge	east	"	2	0	5	0	0	Sum No. of Readings
Height of Observation Pt.	55'	"	3	0	0	5	5	40
Background Description	rust red	"	4	0	5	5	5	Average Opacity
Weather Conditions			5	5	5	5	5	2.25
Wind Direction	SE ± NW	"	6	5	5	5	0	Opacity Range
Wind Speed	0-5	"	7	0	0	0	0	0 % to 5 %
Ambient Temperature	55°F	"	8	0	0	5	5	
Sky Condition (clear, over- cast, % clouds, etc.)	clear	"	9	0	5	0	0	
Plume Description			10	0	0	0	5	
Color	white	"						
Distance Visible	4-5 mi. under puffing							
Other Information								
Comments:								

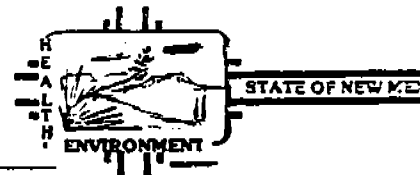
Steve Schuebke
Observer's Signature

Owner or Manager of Operation

IMPORTANT: Please indicate the following by sketch:



ENVIRONMENTAL IMPROVEMENT DIVISION
RECORD OF VISUAL DETERMINATION OF OPACITY



Company Texas Concrete Products
Location El Paso Observer Steve Schuchman
Test Number 2 Observer Certification Date 11-22-80
Date 5-18-81 Observer Affiliation NM EID Air Quality
Type of Facility mill Point of Emission #3 (2nd from east)
Control Device baghouse Height of Discharge Point 30'

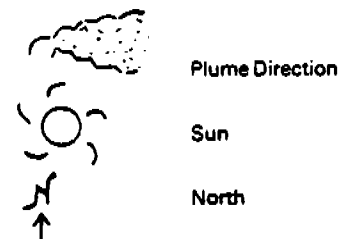
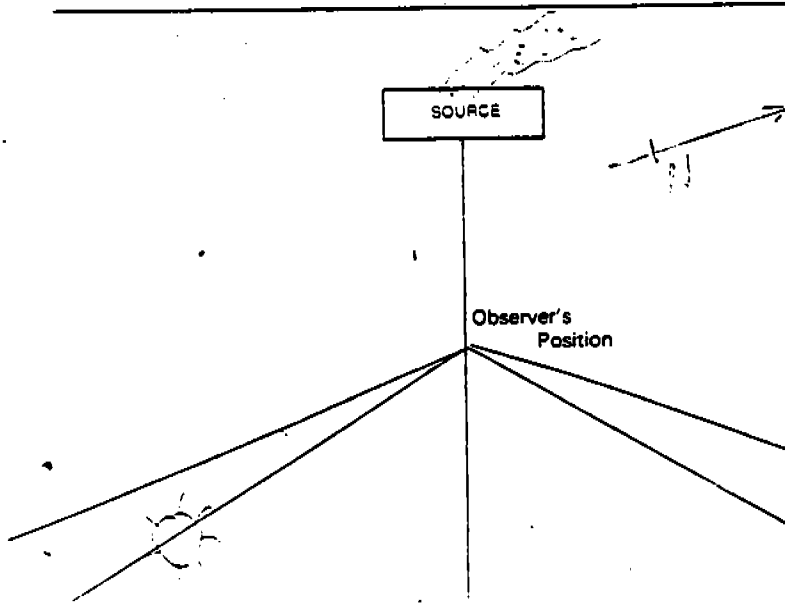
	Initial	Final	Record Opacity in % 5% Smallest Division					OPACITY AVERAGE
Clock Time	12:05	12:16:15	sec min	0	15	30	45	Sum of No. Recorded
Observer Location								
Distance to Discharge	75'	"	1	0	5	5	0	130
Direction from Discharge	east	"	2	0	0	5	10	Sum No. of Readings
Height of Observation Pt.	55'	"	3	10	10	5	10	40
Background Description	rust + tan	"	4	5	5	10	5	Average Opacity
Weather Conditions			5	5	0	0	5	3.25
Wind Direction	SE → NW	"	6	0	0	0	0	Opacity Range
Wind Speed	0 - 10	"	7	0	0	0	0	0 % to 10 %
Ambient Temperature	50°F	"	8	5	5	0	5	
Sky Condition (clear, over- cast, % clouds, etc.)	5° clgy	"	9	0	0	0	0	
Plume Description			10	5	5	0	10	
Color	white	"						
Distance Visible	4-5 ft unless puffing							
Other Information								

Comments: _____

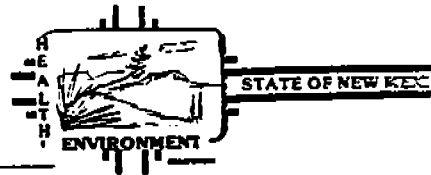
Steve Schuchman
Observer's Signature

Owner or Manager of Operation

IMPORTANT: Please indicate the following by sketch:



ENVIRONMENTAL IMPROVEMENT DIVISION
RECORD OF VISUAL DETERMINATION OF OPACITY



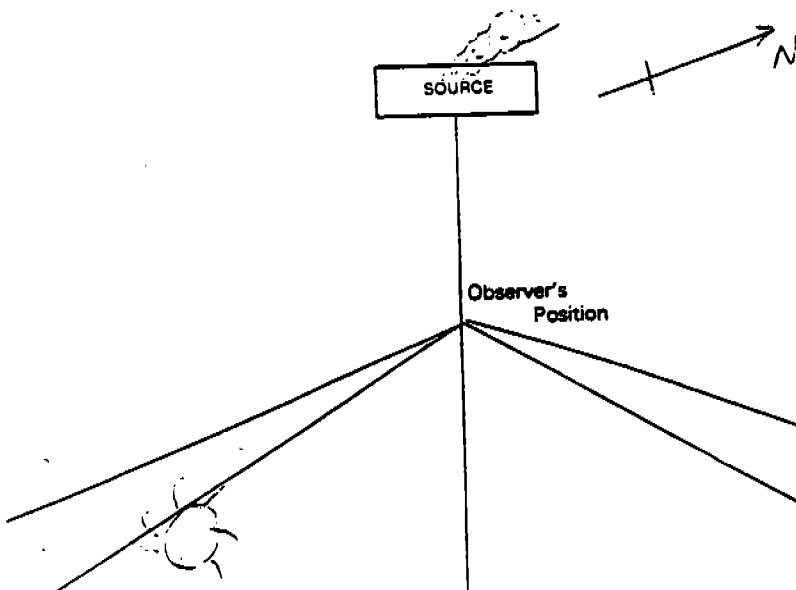
Company Johns Manville Perlite
Location Ala Agua Observer Steve Schwelke
Test Number 1 Observer Certification Date 10-22-80
Date 8-18-81 Observer Affiliation NM EIO Air Quality
Type of Facility Perlite Stack Point of Emission STACK #4 (Cell)
Control Device Baghouse Height of Discharge Point 30'

	Initial	Final	Record Opacity in % 5% Smallest Division					OPACITY AVERAGE		
			sec min	0	15	30	45	Sum of No. Recorded	Sum No. of Readings	
Clock Time.....	11:29	11:40:30								
Observer Location	75'	"	1	0	0	0	0		120	
Distance to Discharge.....			2	0	0	5	5			
Direction from Discharge.....	east	"	3	15	10	5	5			40
Height of Observation Pt.....	55'	"	4	5	0	0	0			
Background Description.....	rust + tan	"	5	5	0	0	5			Average Opacity
Weather Conditions			6	0	0	5	0			3%
Wind Direction.....	SE → NW	"	7	0	0	0	0			
Wind Speed.....	0-5	"	8	0	5	0	10			Opacity Range
Ambient Temperature.....	50°F	"	9	5	5	5	5			0 % to 15 %
Sky Condition (clear, over- cast, % clouds, etc.).....	5% cldy	"	10	5	5	5	5			
Plume Description										
Color.....	white	"								
Distance Visible.....	5 ft. under puffing									
Other Information										
Comments:										

Steve Schwelke
Observer's Signature

Owner or Manager of Operation

IMPORTANT: Please indicate the following by sketch:

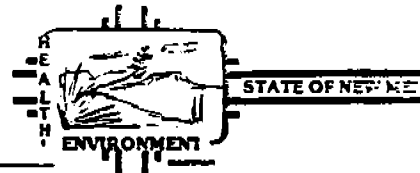


Plume Direction

Sun

North

ENVIRONMENTAL IMPROVEMENT DIVISION
RECORD OF VISUAL DETERMINATION OF OPACITY



Company Johnson Controls Inc.
Location Albuquerque Observer Steve Schuchter
Test Number 1 Observer Certification Date 10-22-80
Date 3-17-81 Observer Affiliation AMA E110 Air Quality
Type of Facility acrylic dryer Point of Emission top of stack (south)
Control Device baghouse Height of Discharge Point 30'

	Initial	Final	Record Opacity in % 5% Smallest Division				OPACITY AVERAGE
			sec min	0	15	30	
Clock Time	4:18	4:27:45					
Observer Location							Sum of No. Recorded
Distance to Discharge	150'	"	1	0	0	0	60
Direction from Discharge	S-SW	"	2	0	0	0	
Height of Observation Pt.	ground	"	3	0	0	0	Sum No. of Readings
Background Description	dry grass	"	4	0	0	10	40
Weather Conditions			5	15	10	5	Average Opacity
Wind Direction	E → W	"	6	5	0	0	1.5
Wind Speed	0-5	"	7	0	0	0	
Ambient Temperature	55°	"	8	0	5	5	Opacity Range
Sky Condition (clear, overcast, % clouds, etc.)	90% H. cl. d.	"	9	0	0	5	0 % to 15 %
Plume Description			10	0	0	0	
Color	white	"					
Distance Visible	30' when visible						

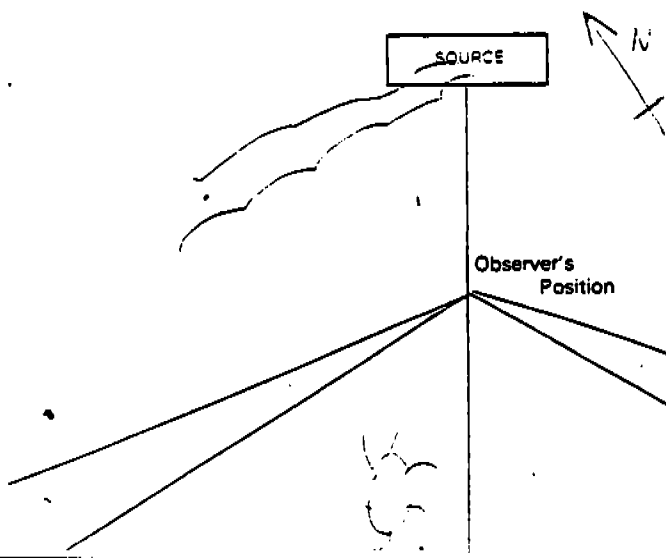
Other Information

Comments:

Steve Schuchter
Observer's Signature

Owner or Manager of Operation

IMPORTANT: Please indicate the following by sketch:



Plume Direction

Sun

North

RESUME OF STACK SAMPLING PERSONNEL

Jimmy T. Romero

Environmental Scientist III
HED/EID/Air Quality Bureau

Education: B.S. 1974, Biology and Chemistry
New Mexico Highlands University
Las Vegas, NM

Certification: Certificate in Propulsion Engineering School
U.S.N. 1969

Training: Air Pollution Training Institute, EPA Course #431,
Air Pollution Control Technology

Air Pollution Training Institute, EPA Course #450,
Source Sampling for Particulate Pollutants

Air Pollution Training Institute, EPA Course #468,
Source Sampling and Analysis for Gaseous Pollutants

Air Pollution Training Institute, EPA Course,
Supervisor and Management Training

Course in Method "9", Visible Emissions and Certification

Experience: 5½ years stack sampling with the State of New Mexico
HED/EID/Air Quality Bureau

Tim Booker

Environmental Technician III
HED/EID/Air Quality Bureau

Education: B.A. 1977, Biology and Psychology
New Mexico Highlands University
Las Vegas, NM

Training: Visible Emission Evaluation Certificate, Method "9"

Air Pollution Training Institute, EPA Course #450,
Source Sampling for Particulate Pollutants

Experience: 2½ years stack sampling with the State of New Mexico
HED/EID/Air Quality Bureau

Mario Romero

Environmental Technician III
HED/EID/Air Quality Bureau

Education: High School Diploma, 1968

Training: Registered with the New Mexico Department of Agriculture
as a pesticide applicator

Visible Emission Evaluation Certificate, Method "9"

Experience: 5 years with the State of New Mexico, Environmental Improvement
Agency in Taos as an Environmental Technician under the CETA
program: 2½ years stack sampling with the State of New Mexico
HED/EID/Air Quality Bureau