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REPORT ON SOURCE TESTS,
VISIBLE EMISSIONS, AND PLANT OBSERVATIONS

Facility Inspection

KAISER STEEL CORPORATION
FONTANA, CALIFORNIA

Coke Oven Battery B

Dates of Inspection

July 26, 1979

Inspected By

Donald Holtz & Robert Tomlinson
Environmental Engineers

Prepared For

U. S. ENVIRONMENTAL PROTECTION AGENCY, REGION IX
215 FREMONT STREET
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Task Order 66/TSA 3
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August 1979

Submitted By

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OBSERVATION OF SOURCE TESTS
AT KAISER STEEL CORPORATION
FONTANA, CALIFORNIA

July 26, 1979

INTRODUCTION

Tests to determine particulate emissions from the baghouse serving Coke Oven Battery B were conducted on the above dates by technical personnel of Environmental Quality Control, Kaiser Steel Corporation. Visual emission observations of the discharge stack were also made during the same period by a South Coast Air Quality Management District Inspector.

The tests and observations were conducted pursuant to Paragraph X of the Amended Consent Decree entered on September 30, 1977 at the U.S. District Court, Central District of California (Case No. CV76-0675MML).

PROCESS DESCRIPTION

Pertinent data for the coke batteries at Kaiser Steel Corporation have been reported previously (see report for Coke Battery E, March 1979). Each oven is charged with about 14 tons of coal from an overhead larry car and heated for 16 to 18 hours to complete the coking process. At the end of this period, the incandescent coke is horizontally pushed from the oven into a receiving ("hot") car for quenching and transfer to the blast furnaces. The pushing is accomplished with a ram which travels on the side of the ovens opposite to the hot car. Charging is done immediately after the expulsion of the coked product.

The ovens of Battery B are heated with coke oven gas, using 110,000 to 165,000 cubic feet per hour of gas of about 550 BTU/ft.³ heat content (the variations in observed gas usage are a function of the charging activity at the battery during the tests). The brick work surrounding the ovens is used for regenerative heating of the combustion air being introduced, employing a reversal cycle every 30 minutes.

SAMPLING AND ANALYTICAL PROCEDURES

The sampling was conducted at the outlet duct of the baghouse at a point upstream of the induced draft fan and stack. The gases travel horizontally across with an approximate 20-foot run prior to the sampling station. The SCAQMD permitted the Kaiser Source Team to conduct two traverses in series through the horizontal sampling port instead of separate traverses through the horizontal and vertical sampling ports. Sampling was done at six points along each traverse with five minute sampling times for each point. Great care was used in the introduction and removal of the sampling probe and nozzle into and from the duct due

to the negative static pressure (7" to 9" H₂O).

The procedure followed EPA Method 5 equipment and procedures, also including the processing of "back-half" (impinger) collection to determine total particulate matter. This was necessary to determine compliance with applicable local regulations (see discussion of Data and Results).

In addition to particulate sampling, samples of gas were aspirated from the duct at five-minute intervals into a 2-cubic foot plastic bag to obtain an integrated average gas sample for each one-hour test. The contents of each bag were analyzed at the laboratory using Horiba MEXA/200 and MEXA/201 infrared analyzers for carbon dioxide and carbon monoxide, respectively, and a Teledyne oxygen analyzer. Nitrogen was determined by difference.

The technique used by Kaiser Steel Corporation personnel during the sampling and sample processing (nozzle-probe, filter, impingers) appeared excellent to this observer. The personnel have many years' experience in sampling for particulates; also, the equipment was in excellent condition and showed careful maintenance. The weighing of the filters and determination of the impinger residue weights was not observed due not only to practical limitations, but also deemed unnecessary because of the competence demonstrated by the laboratory personnel.

DATA AND RESULTS

The test data, calculations, and results as submitted by Kaiser Steel Environmental Quality are included in the Appendix. The particulate matter concentration and emission rates were determined by two methods due to the different regulations promulgated by (a) the former San Bernardino County APCD, and (b) the present SCAQMD. These are as follows:

- (1) Rule 52A: This rule was formerly in effect during the existence of the San Bernardino County APCD. Rule 52A, rather than Rule 404(a) of the SCAQMD (see (2) below), apparently is part of the California SIP as submitted to EPA, hence is still considered effective for compliance determinations. Rule 52A requires all collected particulate matter, liquid or solid, to be included in concentration calculations; i.e., "front-half" plus total condensables in the "back-half" of the Method 5 sampling train. The Rule 52A test results and maximum allowables are shown on Table 1, and are a supplement to the test result summary by Kaiser Steel Corporation at the beginning of the Appendix.
- (2) Rule 404(a): This, the present particulate matter concentration rule of the SCAQMD, requires exclusion of all liquid sulfur compounds from the particulate matter weight. In practical terms, this excludes sulfuric acid which is known to exist as the dihydrate (H₂SO₄·2H₂O) when the impinger residue is evaporated to dryness and desiccated (the determination of H₂SO₄ is made by titration; this yields the most conservative value, as has been determined in analyses over many years by the Los Angeles County APCD laboratories).

- (3) Rule 405 (a): This, the present particulate matter mass flow rate rule of the SCAQMD, is based upon solid particulate matter, as defined by SCAQMD Rule 102. The latter defines solid particulate matter as "particulate matter which exists as a solid at standard conditions". This definition does not exclude any solid particulate matter which may be collected by the "back-half" of EPA Method 5 train. Thus, solid particulate matter as defined by the SCAQMD includes the total front and back-half collection of the sampling train, less sulfuric acid dihydrate [as for Rule 404(a)] Unless the presence of other liquid particulate matter can be shown.

TABLE 1
KAISER STEEL CORPORATION
COKE PLANT BATTERY B COMPLIANCE TEST

RULE 52A RESULTS^(a)

Test No.	Date & Time	Gas Flow Rate (fscfm)	Particulate Matter Concentration Rule 52A - gr/dscf	
			Test ^(b)	Allowed
B-1	7/26/79 0935-1095		Test Discarded	
B-2	7/26/79 1345-1415		Test Discarded	
B-3	3/27/79 0925-1035	34511	.0188	.0516
B-4	3/27/79 1138-1278	39625	.0278	.0497

(a) See Appendix for all other results, data and calculations performed by Environmental Quality Control-Kaiser Steel Corporation.

(b) The variability in Rule 52A concentration, as compared to the Rule 404(a) results, are caused by the differences in the H₂SO₄ content in the "back-half" condensables for the three tests.

All of the Kaiser Steel Corporation calculations were checked and found to be accurate. Tests B-1 and B-2 conducted on 7/26/79 were discarded due to pitot tube error. Water was found in the pitot line after sampling, causing high pitot tube readings.

PROCESS EQUIPMENT OBSERVATIONS

Process equipment observations were recorded by Mr. Eldon Winterbourne of Kaiser Steel.

According to the control instrument setting, the baghouse filter bags are cleaned by reverse and pressure when the pressure drop attains 8 inches of water. One cleaning cycle apparently occurred as 0955 on July 27 during test B-3.

VISIBLE EMISSION OBSERVATIONS

Mr. Robert Bean of the South Coast Air Quality Management District observed emissions from battery B stack during the source tests. His observations are included in the appendix.

The writer and Mr. Al Gubey, SCAQMD, informally observed the stack at intervals and noted visible emissions of 0% opacity at those times. The battery B baghouse transmissometer was not on line during the tests because the contractor had not yet satisfied the operation/calibration contract specifications.

APPENDIX

Summary - Kaiser Steel Corporation Battery B
Compliance Tests

Compliance Test Notes

Test B-3

Particulate Field Data
Laboratory Analysis Data
Calculations

Test B-4

Particulate Field Data
Laboratory Analysis Data
Calculations

Visual Emission Observations

All Tests: Robert Bean SCAQMD

Baghouse Process Data

TEST RESULTS
XSC - COKE PLANT BATTERY "B" BAGHOUSE

DATE TIME	TEST NO. *	EXHAUST GAS		Rule 404(a) Concentration		Rule 405(a) Solid Particulate		% Isokinetic	Baghouse Average Δp "H ₂ O
		ACFM	OF	Allowable gr/dscf	Actual gr/dscf	Allowable lbs/hr	Actual lbs/hr		
7/27/79 0925-1035	B-3	69044 34511	415	0.0498 @34511 dscfm	0.0114	13.4 @35,000 lb/hr proc.wt.	3.29	96.4	6.48
7/27/79 1138-1238	B-4	79219 39625	407	0.0473 @39625 dscfm	0.0151	13.4 @35,000 lb/hr proc.wt.	4.60	91.50	6.96

*Tests B-1 and B-2 run on 7/26/79 discarded due to pitot tube error. Water was found in impact line after sampling causing high pitot tube readings.

JAM:pw
8/1/79

Btry. "B" Compliance Test Notes.

I. Test B-1, 7/26/79, 0936-1036

- (1) Post leak check OK - < 0.01 cfm @ 7.2°Hg .
- (2) Pitot reading went to above $1.0^{\circ}\text{H}_2\text{O}$ after 10 minutes and stayed very constant.

II. Test B-2, 7/26/79, 1345-1445

- (1) Post leak check indicated 0.06 cfm leak @ 5.5°Hg .
- (2) Pitot reading went to above $1.00^{\circ}\text{H}_2\text{O}$ within 15 minutes and stayed constant for remainder of test.
- (3) Ran out of ice for impingers, temp. up to 81°F .
- (4) Difficulty in maintaining sample box and probe temperature. Sample box range ($219-275^{\circ}\text{F}$), Probe range ($156-291^{\circ}\text{F}$).

III. Test B-3, 7/27/79, 0925-1035

- (1) Post leak check OK - 0.01 cfm @ 4.5°Hg .
- (2) Changed umbilical cord.
- (3) Could not keep impingers below 70°F .
Suspect faulty impinger T.C. had plenty of ice in system.

IV. Test B-4, 7/27/79, 1138-1238.

- (1) Post leak check indicated 0.04 cfm leak @ 5.2°Hg .
- (2) Could not maintain impinger temperature below 70°F . Suspect bad T.C.

General

- (1) Checked umbilical cord used on 7/26/79 and found about 6.5 cc of water in the pitot tube impact line. Pitot readings were faulty on 7/26/79. The samples on 7/26/79 were not taken at an isokinetic sampling rate due to the pitot tube problem.
- (2) Checked umbilical cord used on 7/27/79 and did not find any water in pitot lines.

V. Rule 404(a) Straight Line Interpolation

Test B-1 Exhaust Volume = 47503 dscfm

@ 45910 dscfm allowable = 0.0445 gr/dscf

@ 49440 dscfm allowable = 0.0437 gr/dscf

Allowable @ 47503 dscfm =

$$0.0445 - (0.0445 - 0.0437) \frac{(47503 - 45910)}{(49440 - 45910)}$$

$$= 0.0445 - 0.00036$$

$$= 0.04414 \text{ round off to } \underline{\underline{0.0441}}$$

V-Contd: Rule 404(a) Straight Line Interpolation

Test B-2 Exhaust Volume = 46420 dscfm

@45910 dscfm allowable = 0.0445 gr/dscf

@49440 dscfm allowable = 0.0437 gr/dscf

Allowable @46420 dscfm =

$$0.0445 - (0.0445 - 0.0437) \frac{(46420 - 45910)}{(49440 - 45910)}$$

$$= 0.0445 - 0.00012$$

$$= 0.04438 \text{ round off to } 0.0444 \text{ gr/dscf}$$

Test B-3 Exhaust Volume = 34511 dscfm

@31780 dscfm allowable = 0.0515 gr/dscf

@35310 dscfm allowable = 0.0493 gr/dscf

Allowable @34511 dscfm =

$$0.0515 - (0.0515 - 0.0493) \frac{(34511 - 31780)}{(35310 - 31780)}$$

$$= 0.0515 - 0.0017$$

$$= 0.0498 \text{ gr/dscf @34511 dscfm}$$

Test B-4 Exhaust Volume = 39625 dscfm

@38850 dscfm allowable = 0.0476 gr/dscf

@42380 dscfm allowable = 0.0463

Allowable @ 39625 dscfm

$$= 0.0476 - (0.0476 - 0.0463) \frac{(39625 - 38850)}{(42380 - 38850)}$$

$$= 0.0476 - 0.00028$$

$$= 0.04732 \text{ round off to } 0.0473 \text{ gr/dscf}$$

VI Rule 405(a) Allowable Rate based on Process Weight.

7/26/79 29 charges of 14 tons each

VI-Contd: Rule 405(a) Allowable Rate based on Process Weight.

$$\text{Process wt.} = \frac{29 \times 14 \times 2000}{24} = 33,833 \text{ lbs/hr}$$

Table 405(a)

@33,070 lbs/hr allowable = 13.2 lbs/hr.

@38,580 lbs/hr allowable = 13.7 lbs/hr.

Allowable @33,833 lbs/hr.

$$= 13.2 + (13.7-13.2) \frac{(33833-33070)}{(38580-33070)}$$

$$= 13.2 + 0.07 = 13.27 \text{ Round off to } \underline{13.3 \text{ lbs/hr}}$$

7/27/79 30 charges of 14 tons each

$$\text{Process wt.} = \frac{30 \times 14 \times 2000}{24} = 35,000 \text{ lbs/hr.}$$

Allowable @35,000 lbs/hr.

$$= 13.2 + (13.7-13.2) \frac{(350000-33070)}{(38580-33070)}$$

$$= 13.2 + 0.18 = 13.38 \text{ round off to } \underline{13.4 \text{ lbs/hr.}}$$

VII. Stack height shown on visible emission observation sheets should be 225' not 125'.

JAM:pw
8/1/79

Plant ACC - Coke Plant
 Run No. 8-2
 Location East of Warehouse
 Date 7/27/69
 Operator R. F. Heltz

Start Time 0925
 Stop Time 1035
 Ambient Temp. 80
 Barom. Press. "Hg 28.95
 Nozzle Diam. In. 8'
 Probe Length 8'

Sample Box No. 21
 Meter Box No. 2
 Meter ΔH 1.25
 Heater Box Setting, of 250
 Probe Heater Setting, of 250
 Leak Rate @ "Hg 4.5 Post-Test 2.01
 ΔH 1.25 = 2.245 $\times \Delta P$

POINT	TIME MIN.	GAS VOLUME CF	PITOT ΔP "H ₂ O	ORIF. ΔH "H ₂ O	STACK TEMP. OF	BOX TEMP OF	IMP. TEMP. OF	PROBE TEMP. OF	DRY GAS TEMP. - OF		PUMP VAC. "Hg	STACK S.P. "H ₂ O
									IN	OUT		
S-6	0	492.8	0.54	1.21	405	260	81	274	82	74	4.2	-10.4
S-5	5	495.8	0.58	1.30	418	263	78	284	89	75	4.2	
S-4	10	498.9	0.58	1.30	419	249	76	229	93	78	4.2	
S-3	15	502.1	0.58	1.30	417	235	75	274	97	80	4.2	
S-2	20	505.2	0.54	1.21	417	264	77	269	100	83	4.1	
S-1	25	506.2	0.40	0.90	409	260	84	292	103	86	3.3	
S-6	30	510.8	0.54	1.21	412	248	78	289	105	88	4.0	
S-5	35	513.8	0.60	1.34	417	236	75	257	107	91	4.3	
S-4	40	517.0	0.60	1.34	419	261	73	241	108	92	4.3	
S-3	45	520.2	0.58	1.30	449	268	75	227	110	94	4.2	
S-2	50	523.4	0.52	1.17	416	246	76	239	111	96	3.3	-10.5
S-1	55	526.4	0.38	0.85	407	245	80	253	112	98		
	60	529.0							ave	ave		ave
			ave ΔP	ave ΔH	ave Temp				101	86		-10.45
			$\sum = 36.2$	$= 0.731$	$= 1.20$	$= 4154$						

TEST OBSERVERS:
 Byg Tomlinson - EST - EPA
 All Givney - SCA-01110

COMMENTS:

GAS VEL., fps
 VOLUME, dscfm
 MOISTURE, %

PART. gr/dscf lb/hr
 TOTAL
 NET
 SOLID

LABORATORY ANALYSIS DATA
PARTICULATE SOURCE SAMPLE

Analysis Date(s) 7/30/79 + 7/31/79 Analytical Chemist Samuel Deutsch
Sample Date 7/27/79 Run No. B-3 Location CO. "B" STACK BAGHOUSE
Lab. No. 40893

MOISTURE DATA:

Final Vol. H₂O in Imp. 275 ml. 5. Final Wt. Silica Gel 808.50 gm.
Initial Vol. H₂O in Imp. 200 ml. 6. Initial Wt. Silica Gel 798.40 gm.
Vol. H₂O Condensed 75 ml. 7. Weight Gain 10.10 gm.
Vol. wash H₂O 150 ml.

ARTICULATE DATA:

(Front Half:)

(Back Half:)

Final Filter Weight 354.3 mg. 13. Organic Extract 0.5 mg.
Initial Filter Weight 338.4 mg. 14. Aqueous Insolubles 0.2 mg.
Filter Particulate 15.9 mg. 15. Aqueous Solubles 19.2 mg.
Probe Particulate 4.3 mg. 16. Total Particulate 19.9 mg.
Total Particulate 20.2 mg. 17. H₂SO₄·2H₂O 15.8 mg.
18. Net Particulate 4.1 mg.
Acetone Wash 30 ml.

FLUE GAS ANALYSES

Molecular Weight Determination:

Room Temp. 77°F Barom. Press. 28.92" Hg

Component
10. %CO₂ 4.4 @ 3.2% H₂O % Dry
11. %O₂ 15.5 " 4.55
12. %CO 0.05 " 16.01
13. %N₂ 79.39 0.05
Horiba Moxa 204 IR Analyzer
Tetalyne O₂ Analyzer
Horiba Moxa 201 IR Analyzer
by Difference

Other

24. _____
25. _____
26. _____

METHOD 5 PARTICULATE TEST CALCULATION FORM

LOCATION

KSC - Coke Plant Battery "B"

DATE

7/27/79

RUN NO.

B-3

I. Necessary Data:

A. No. of traverse points 6B. Total test time, (t) 60 minutes

C. Water collected:

1. Impinger H₂O; V_{H₂O} 75 ml.2. Silica Gel, W_{H₂O} 10.10 gm.

D. Particulate Weight:

1. Front Half, M_F 0.0202 gm.2. Back Half, M_B 0.0179 gm.3. Back Half H₂SO₄·2H₂O 0.0153 gm.4. Back Half Organic, M_O 0.0005 gm.

E. Volume metered

 $V_m = \frac{36.2}{1} \text{ CF} \times \text{DMCF} = 36.2 \text{ CF}$ F. Average $\sqrt{\Delta P}$ 0.731 ("H₂O)^{1/2}G. Average ΔH 1.20 "H₂O/13.6 = 0.088 "HgH. Average meter temperature, T_m 94 °F + 460 = 554 °RI. Average stack temperature, T_s 415 °F + 460 = 875 °RJ. Stack absolute pressure, P_s 28.18 "HgK. Stack static pressure -10.45 "H₂OL. Barometric pressure, P_b 28.95 "HgM. % CO₂ 4.55; % O₂ 16.01; % CO 0.05; % N₂ 79.39N. Area of stack, A_s 20.63 ft²O. Area of nozzle, A_n 0.000341 ft²P. Pitot tube factor, C_p 0.35

II. Calculations:

A. Standard Volume Metered

$$V_{m(std)} = V_m \times \frac{T_{std}}{P_{std}} \times \frac{(P_b + \frac{H}{13.6})}{T_m}$$

$$V_{m(std)} = 17.380 \times (\underline{36.2} \text{ CF}) \times \frac{(\underline{29.04} \text{ "Hg})}{(\underline{554} \text{ } ^\circ\text{R})} = \underline{32.98} \text{ dscf}$$

B. Moisture Content of Stack Gas

1. H₂O collected in impingers

$$V_{wc(std)} = K (V_{H_2O})$$

$$V_{wc(std)} = 0.04636 \times (\underline{75} \text{ ml.}) = \underline{3.48} \text{ scf}$$

2. H₂O collected in silica gel

$$V_{wsg(std)} = K \times (V_{H_2O})$$

$$V_{wsg(std)} = 0.04644 \times (\underline{10.10} \text{ gm.}) = \underline{0.47} \text{ scf}$$

3. Moisture Content of Stack Gas, B_{ws}

$$B_{ws} = \frac{V_{wc(std)} + V_{wsg(std)}}{V_{wc(std)} + V_{wsg(std)} + V_{m(std)}}$$

$$B_{ws} = \frac{(\underline{3.48} \text{ scf}) + (\underline{0.47} \text{ scf})}{(\underline{3.48} \text{ scf}) + (\underline{0.47} \text{ scf}) + (\underline{32.98} \text{ scf})} = \underline{0.107}$$

C. Molecular Weight of Stack Gas, lb/lb-mole

1. M_d (Dry Molecular Weight) = $\sum M_x B_x$

$$M_d = (0.44) \underline{4.55} \% \text{ CO}_2 + (0.32) \underline{16.01} \% \text{ O}_2 + (0.28) \underline{79.44} \% (\text{N}_2 + \text{CO})$$

$$= \underline{29.37} \text{ lb/lb-mole}$$

2. M_s (Wet Molecular Weight) = M_d (1 - B_{ws}) + 18 B_{ws}

$$M_s = (\underline{29.37}) (1 - \underline{0.107}) + 18 (\underline{0.107}) = \underline{28.15} \text{ lb/lb-mole}$$

D. Average Stack Gas Velocity

$$\bar{V}_s = K_p C_p \left(\frac{T_s}{P_s M_s} \right)^{\frac{1}{2}} \sqrt{\Delta P}$$

$$\bar{V}_s = 85.48 (\underline{0.85}) \left[\frac{(\underline{875} \text{ } ^\circ\text{R})}{(\underline{28.13} \text{ "Hg}) (\underline{28.15} \text{ lb/mole})} \right]^{\frac{1}{2}} (\underline{0.731} \text{ "H}_2\text{O}^{\frac{1}{2}})$$

$$= \underline{55.78} \text{ ft/sec}$$

$$\text{acfm} = 55.78 \times 60 \times 20.63 = 69,044 \text{ acfm}$$

E. Average Stack Gas Volumetric Flow Rate

$$\bar{Q}_s = (3600 \text{ sec/hr}) \bar{V}_s A_s (1 - B_{ws}) \frac{T_{std}}{P_{std}} \frac{P_s}{T_s}$$

$$= 62566.8 (55.78 \text{ ft/sec}) (20.63 \text{ ft}^2) (1 - 0.107) \frac{(28.18 \text{ "Hg})}{(875 \text{ }^\circ\text{R})}$$

$$= 2,070,647 \text{ dscfh/60} = 34,511 \text{ dscfm}$$

F. Pollutant Mass Rate (Solid Part.- Rule 405a)

$$\text{PMR} = \frac{M_f + M'}{V_{m(\text{std})}} \times \bar{Q}_s$$

$$M' = M_b - M_o - (H_2SO_4 \cdot 2H_2O)$$

$$M' = 0.0199 - 0.0005 - 0.0153$$

$$M' = 0.0036$$

$$\text{PMR} = \frac{(0.0238 \text{ gm})}{(32.98 \text{ dscf})} \times (2,070,647 \text{ dscfh}) \times \frac{1}{454 \text{ gm/lb}}$$

$$= 3.29 \text{ lb/hr}$$

G. Particulate Concentration

1. Total Particulate

$$C_t = \frac{M_f + M_b}{V_{m(\text{std})}} \times 15.43$$

$$C_t = \frac{(0.0202 \text{ gm}) + (0.0199 \text{ gm})}{(32.98 \text{ dscf})} \times 15.43 = 0.0188 \text{ gr/dscf}$$

2. Net Particulate (Total less $H_2SO_4 \cdot 2H_2O$ - Rule 404a)

$$C_n = \frac{M_f + M_b - (H_2SO_4 \cdot 2H_2O)}{V_{m(\text{std})}} \times 15.43$$

$$C_n = \frac{(0.0202 \text{ gm}) + (0.0199 \text{ gm}) - (0.0153 \text{ gm})}{(32.98 \text{ dscf})} \times 15.43$$

$$= 0.0114 \text{ gr/dscf}$$

3. Front Half Particulate

$$C_f = \frac{M_f}{V_{m(\text{std})}} \times 15.43$$

$$C_f = \frac{(0.0202 \text{ gm})}{(32.98 \text{ dscf})} \times 15.43 = 0.0094 \text{ gr/dscf}$$

H. % Isokinetic Variation

$$\% I = \frac{T_s V_m(\text{std}) P_{\text{std}} \times 100}{\theta \bar{V}_s A_n P_s T_{\text{std}} (1 - B_{ws}) \times 60}$$

$$\% I = 0.0959 \times \frac{(\underline{875}^{\circ}\text{R})(\underline{32.93} \text{ dscf})}{(\underline{60} \text{ min})(\underline{55.78} \text{ ft/sec})(\underline{0.00341} \text{ ft}^2)(\underline{28.13} \text{ "Hg})(1 - \underline{0.107})}$$

$$= \underline{96.4\%}$$

(Std Conditions: 60 °F and 29.92 "Hg)

PARTICULATE FIELD DATA

Plant KSC - Coke Plant
 Run No. 8-4
 Location Exit B" Baghouse
 Date 7/27/79
 Operator J. A. Thurnham
RF No. 12

Start Time 1138
 Stop Time 1238
 Ambient Temp. 93
 Barom. Press. "Hg 28.92
 Nozzle Diam. In. 0.250
 Probe Length 8'

Sample Box No. 1
 Meter Box No. 2
 Meter ΔH 1.80
 Heater B6x Setting, OF 250
 Probe Heater Setting, OF 250
 Leak Rate @ "Hg 5.22 Post-Test 0.04
CH 100% = 2.243 AD

POINT	TIME MIN.	GAS VOLUME CF	PITOT ΔP "H ₂ O	ORIF. ΔH "H ₂ O	STACK TEMP. OF	BOX TEMP. OF	IMP. TEMP. OF	PROBE TEMP. OF	DRY GAS TEMP. - OF		PUMP VAC. "Hg	STACK S.P. "H ₂ O
									IN	OUT		
S-6	0	529.8	0.74	1.63	409	231	83	304	95	86	4.5	-11.1
S-5	5	532.7	0.78	1.75	414	260	73	210	100	88	4.8	
S-4	10	536.4	0.78	1.75	413	269	74	229	104	90	4.8	
S-3	15	540.0	0.82	1.84	414	245	71	241	103	93	5.2	
S-2	20	543.8	0.76	1.71	411	226	70	235	110	95	5.0	
S-1	25	547.5	0.45	1.01	383	252	79	258	112	96	3.5	
S-6	30	550.3	0.72	1.62	412	267	77	227	115	99	4.6	
S-5	35	552.7	0.74	1.66	413	281	75	243	116	100	4.8	
S-4	40	554.3	0.76	1.71	412	259	72	253	116	100	5.0	
S-3	45	561.0	0.78	1.75	411	249	71	275	117	102	5.2	
S-2	50	564.6	0.78	1.75	412	238	70	272	118	103	5.2	
S-1	55	568.4	0.45	1.01	383	253	60	237	119	105	3.6	-11.1
	60	571.2							ave	ave		ave
			ave VP	ave ΔH	ave Temp				111	96		-11.1
			$V_p = 41.4$	$= 0.841$	$= 401\%$				104			
			corr. V_p									
			see encls.									

COMMENTS:

TEST OBSERVERS:

PART. gr/dscf 1b/hr
 TOTAL
 NET
 SOLID

GAS VEL., fps
 VOLUME, dscfm
 MOISTURE, %

Bob Tomlinson EST. 12/21/79
 Al Guberg - SCA QM 10

LABORATORY ANALYSIS DATA
PARTICULATE SOURCE SAMPLE

Analysis Date(s) 7/30/74 + 7/30/79 Analytical Chemist Jamuel Deutch
Sample Date 7/27/79 Run No. B-4 Location C.O. "B" Stack Baghouse
Lab. No. 40395

WET WEIGHT DATA:

Final Vol. H ₂ O in Imp.	<u>288</u> ml.	5. Final Wt. Silica Gel	<u>792.60</u> gm.
Initial Vol. H ₂ O in Imp.	<u>200</u> ml.	6. Initial Wt. Silica Gel	<u>782.85</u> gm.
Vol. H ₂ O Condensed	<u>88</u> ml.	7. Weight Gain	<u>9.75</u> gm.
Vol. wash H ₂ O	<u>260</u> ml.		

PARTICULATE DATA: (Front Half:)

1. Final Filter Weight	<u>372.9</u> mg.
2. Initial Filter Weight	<u>351.7</u> mg.
3. Filter Particulate	<u>21.2</u> mg.
4. Probe Particulate	<u>6.5</u> mg.
5. Total Particulate	<u>27.7</u> mg.
6. Acetone Wash	<u>112</u> ml.

(Back Half:)

13. Organic Extract	<u>3.6</u> mg.
14. Aqueous Insolubles	<u>0.6</u> mg.
15. Aqueous Solubles	<u>32.9</u> mg.
16. Total Particulate	<u>37.1</u> mg.
17. H ₂ SO ₄ ·2H ₂ O	<u>29.6</u> mg.
18. Net Particulate	<u>7.5</u> mg.

FLUE GAS ANALYSES

Molecular Weight Determination:

Component	% Dry
20. %CO ₂	<u>4.8</u> @ 3.2% H ₂ O <u>4.96</u>
21. %O ₂	<u>14.9</u> @ 3.2% H ₂ O <u>15.39</u>
22. %CO	<u>0.05</u> " " <u>0.05</u>
23. %N ₂	<u>79.60</u>

Room Temp. 77°F Barom. Press. 23.92" Hg

Horiba Mexa 204 IR Analyzer
Teledyne O₂ Analyzer
Horiba Mexa 201 IR Analyzer
by difference

Other

24.	_____
25.	_____
26.	_____

METHOD 5 PARTICULATE TEST CALCULATION FORM

LOCATION KSC - Coke Plant Battery "B"DATE 7/27/79RUN NO. B-4

Ed. 5 "Pret"

I. Necessary Data:

- A. No. of traverse points 6
- B. Total test time, (t) 60 minutes
- C. Water collected:
1. Impinger H₂O; V_{H₂O} 88 ml.
 2. Silica Gel, W_{H₂O} 9.75 gm.
- D. Particulate Weight:
1. Front Half, M_F 0.0277 gm.
 2. Back Half, M_B 0.0371 gm.
 3. Back Half H₂SO₄·2H₂O 0.0296 gm.
 4. Back Half Organic, M_O 0.0036 gm.
- E. Volume metered $\bar{V}_m$

$$\bar{V}_m = \underline{40.2} \text{ CF} \times \text{DMCF} = \underline{40.2} \text{ CF}$$

F. Average $\sqrt{\Delta P}$ 0.841 ("H₂O)^{1/2}

G. Average ΔH 1.60 "H₂O/13.6 = 0.118 "Hg

H. Average meter temperature, T_m 104 °F + 460 = 564 °R

I. Average stack temperature, T_s 407 °F + 460 = 867 °R

J. Stack absolute pressure, P_s 28.10 "Hg

K. Stack static pressure -11.1 "H₂O

L. Barometric pressure, P_b 28.92 "Hg

M. % CO₂ 4.96 ; % O₂ 15.39 ; % CO 0.05 ; % N₂ 79.60

N. Area of stack, A_s 20.63 ft²

O. Area of nozzle, A_n 0.000341 ft²

P. Pitot tube factor, C_p 0.85

* Note: Total Water Volume
= 41.4 cf
Adjusted for 0.04 cfm leak
by subtracting 1/2 of leak
Corr. V_m = 41.4 - (60)(1/2)(0.04)
= 40.2 cf

II. Calculations:

A. Standard Volume Metered

$$V_{m(std)} = V_m \times \frac{T_{std}}{P_{std}} \times \frac{(P_b + \frac{H}{13.6})}{T_m}$$

$$V_{m(std)} = 17.380 \times (40.2 \text{ CF}) \times \frac{(29.04 \text{ "Hg})}{(564 \text{ } ^\circ\text{R})} = 35.97 \text{ dscf}$$

B. Moisture Content of Stack Gas

1. H₂O collected in impingers

$$V_{wc(std)} = K (V_{H_2O})$$

$$V_{wc(std)} = 0.04636 \times (88 \text{ ml.}) = 4.08 \text{ scf}$$

2. H₂O collected in silica gel

$$V_{wsg(std)} = K \times (W_{H_2O})$$

$$V_{wsg(std)} = 0.04644 \times (9.75 \text{ gm.}) = 0.45 \text{ scf}$$

3. Moisture Content of Stack Gas, B_{ws}

$$B_{ws} = \frac{V_{wc(std)} + V_{wsg(std)}}{V_{wc(std)} + V_{wsg(std)} + V_{m(std)}}$$

$$B_{ws} = \frac{(4.08 \text{ scf}) + (0.45 \text{ scf})}{(4.08 \text{ scf}) + (0.45 \text{ scf}) + (35.97 \text{ scf})} = 0.112$$

C. Molecular Weight of Stack Gas, lb/lb-mole

1. M_d (Dry Molecular Weight) = $\sum M_x B_x$

$$M_d = (0.44) 44.01 \text{ CO}_2 + (0.32) 32.00 \text{ O}_2 + (0.28) 28.01 \text{ (N}_2 + \text{CO)} \\ = 29.41 \text{ lb/lb-mole}$$

2. M_s (Wet Molecular Weight) = M_d (1 - B_{ws}) + 18 B_{ws}

$$M_s = (29.41) (1 - 0.112) + 18 (0.112) = 23.13 \text{ lb/lb-mole}$$

D. Average Stack Gas Velocity

$$\bar{V}_s = K_p C_p \left(\frac{T_s}{P_s M_s} \right)^{\frac{1}{2}} \sqrt{\Delta P}$$

$$\bar{V}_s = 85.43 (0.35) \left[\frac{(867 \text{ } ^\circ\text{R})}{(23.10 \text{ "Hg}) (23.13 \text{ lb/mole})} \right]^{\frac{1}{2}} (0.341 \text{ "H}_2\text{O}^{\frac{1}{2}}) \\ = 64.00 \text{ ft/sec}$$

$$\text{actm} = 64.0 \times 60 \times 20.63 = 79,219 \text{ actm}$$

E. Average Stack Gas Volumetric Flow Rate

$$\bar{Q}_s = (3600 \text{ sec/hr}) \bar{V}_s A_s (1 - B_{ws}) \frac{T_{std}}{P_{std}} \frac{P_s}{T_s}$$

$$= 62566.8 (64.00 \text{ ft/sec}) (20.63 \text{ ft}^2) (1 - 0.112) \frac{(28.10 \text{ "Hg})}{(867 \text{ }^\circ\text{R})}$$

$$= \underline{2,377,515} \text{ dscfh/60} = \underline{39,625} \text{ dscfm}$$

F. Pollutant Mass Rate (Solid Part: - Rule 405a)

$$PMR = \frac{M_f + M'}{V_m(\text{std})} \times \bar{Q}_s$$

$$M' = M_b - H_2O - (H_2SO_4 \cdot 2H_2O)$$

$$M' = 0.0371 - 0.0036 - 0.0296$$

$$M' = 0.0039$$

$$PMR = \frac{(0.0316 \text{ gm.})}{(35.97 \text{ dscf})} \times (2,377,515 \text{ dscfh}) \times \frac{1}{454 \text{ gm/lb}}$$

$$= \underline{4.60} \text{ lb/hr}$$

G. Particulate Concentration

1. Total Particulate

$$C_t = \frac{M_f + M_b}{V_m(\text{std})} \times 15.43$$

$$C_t = \frac{(0.0277 \text{ gm}) + (0.0371 \text{ gm})}{(35.97 \text{ dscf})} \times 15.43 = \underline{0.0278} \text{ gr/dscf}$$

2. Net Particulate (Total less $H_2SO_4 \cdot 2H_2O$ - Rule 404a)

$$C_n = \frac{M_f + M_b - (H_2SO_4 \cdot 2H_2O)}{V_m(\text{std})} \times 15.43$$

$$C_n = \frac{(0.0277 \text{ gm}) + (0.0371 \text{ gm}) - (0.0296 \text{ gm})}{(35.97 \text{ dscf})} \times 15.43$$

$$= \underline{0.0151} \text{ gr/dscf}$$

3. Front Half Particulate

$$C_f = \frac{M_f}{V_m(\text{std})} \times 15.43$$

$$C_f = \frac{(0.0277 \text{ gm})}{(35.97 \text{ dscf})} \times 15.43 = \underline{0.0119} \text{ gr/dscf}$$

H. % Isokinetic Variation

$$\% I = \frac{T_s V_m(\text{std}) P_{\text{std}} \times 100}{\theta \bar{V}_s A_n P_s T_{\text{std}} (1 - B_{ws}) \times 60}$$

$$\% I = 0.0959 \times \frac{(867 \text{ } ^\circ\text{R})(35.97 \text{ dscf})}{(60 \text{ min})(64.00 \text{ ft/sec})(0.00034 \text{ ft}^2)(28.10 \text{ "Hg})(1 - 0.112)}$$

$$= \underline{91.50\%}$$

(Std Conditions: 60 °F and 29.92 "Hg)

VISIBLE EMISSION OBSERVATION RECORD

Company KAISER STEEL CORP RUN # 1

Date 7-27-79 Time First Sighted Plume 0

Time Start 0925 Time Stop 1025

Air Temperature 77° Relative Humidity

Wind Speed 3-5 MPH Wind Direction 200°

Sky Condition CLEAR Background HAZY

Plume Characteristics: Continuous: () yes (✓) no

Color 0 Dispersion Description 0

Stack Height 125 (ft) Observer location: 900 (ft) SE of stack

Sun location
 () Back of Observer () Left Shoulder
 (✓) Right Shoulder () Other

Emission Point BATTERY "B" STACK

Min	0	15	30	45
01	0	0	0	0
02	0	0	0	0
03	0	0	0	0
04	0	0	0	0
05	0	0	0	0
06	0	0	0	0
07	0	0	0	0
08	0	0	0	0
09	0	0	0	0
10	0	0	0	0
11	0	0	0	0
12	0	0	0	0
13	0	0	0	0
14	0	0	0	0
15	0	0	0	0
16	0	0	0	0
17	0	0	0	0
18	0	0	0	0
19	0	0	0	0
20	0	0	0	0

Min	0	15	30	45
21	0	0	0	0
22	0	0	0	0
23	0	0	0	0
24	0	0	0	0
25	0	0	0	0
26	0	0	0	0
27	0	0	0	0
28	0	0	0	0
29	0	0	0	0
30	0	0	0	0
31	0	0	0	0
32	0	0	0	0
33	0	0	0	0
34	0	0	0	0
35	0	0	0	0
36	0	0	0	0
37	0	0	0	0
38	0	0	0	0
39	0	0	0	0
40	0	0	0	0

Min	0	15	30	45
41	0	0	0	0
42	0	0	0	0
43	0	0	0	0
44	0	0	0	0
45	0	0	0	0
46	0	0	0	0
47	0	0	0	0
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49	0	0	0	0
50	0	0	0	0
51	0	0	0	0
52	0	0	0	0
53	0	0	0	0
54	0	0	0	0
55	0	0	0	0
56	0	0	0	0
57	0	0	0	0
58	0	0	0	0
59	0	0	0	0
60	0	0	0	0

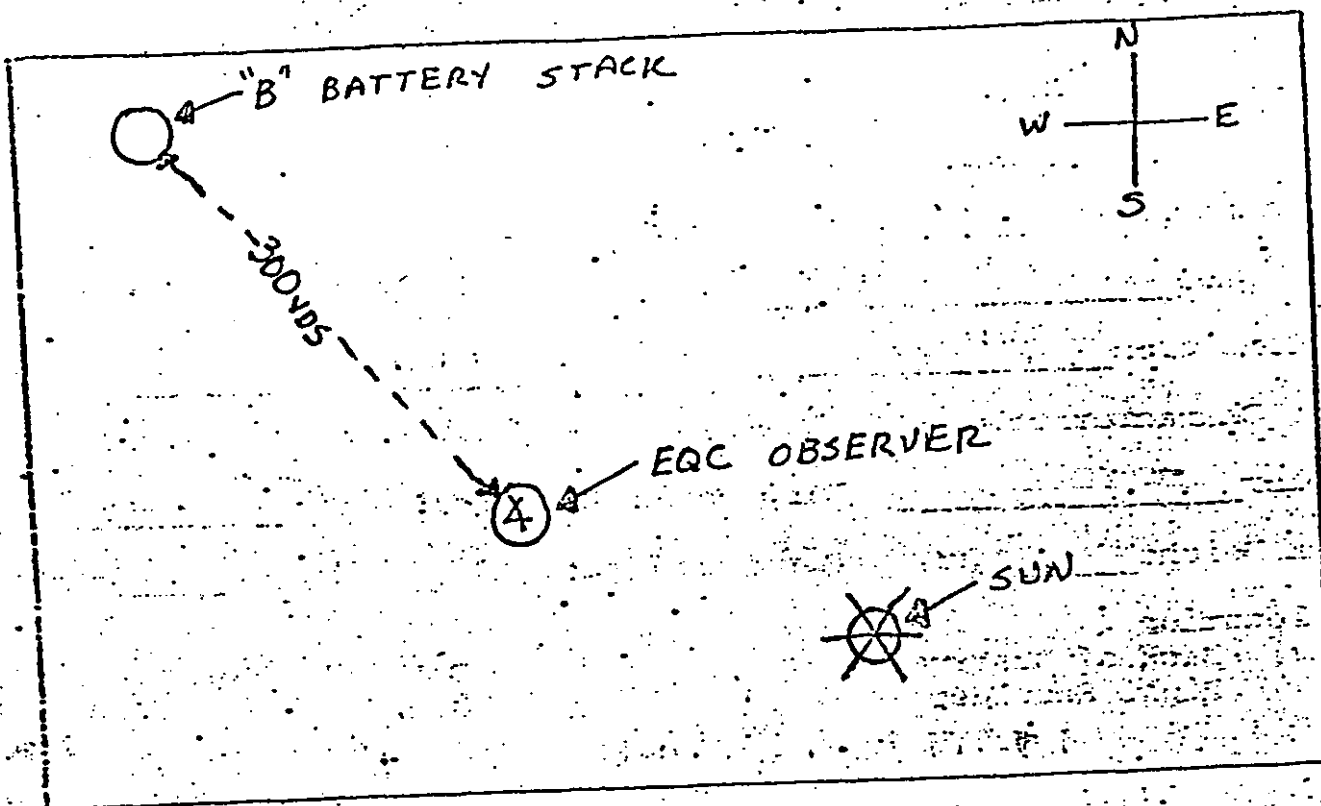
NOTES: NO VISIBLE EMISSIONS.

Inspector R. L. Skipper Date 7-27-79

TSB-A-8 EPA-1A-FORM 208 Certified by C.A.R.D. 5-10-79

MAP

09.25 - 1025



Symbols

Sun =

Plume direction =

Point where plume observed =

Observer =

Water Vapor Condensate _____

Photographs: S&A File () Enclosed () None ()

Comments _____

Signature R. L. Skypen Date 7-27-79

VISIBLE EMISSION OBSERVATION RECORD

Company KAISER STEEL Run # 2

Date 7-27-79 Time First Sighted Plume _____

Time Start 1140 Time Stop 1240

Air Temperature 90° Relative Humidity _____

Wind Speed 8-11 MPH Wind Direction 224°

Sky Condition CLEAR Background HAZY

Plume Characteristics: Continuous: () yes () no

Color _____ Dispersion Description _____

Stack Height 125 (ft) Observer location: 900 (ft) SE of stack

Sun location
☒ Back of Observer
☐ Right Shoulder
☐ Left Shoulder
☐ Other

Emission Point _____

Min	0	15	30	45
01	0	0	0	0
02	0	0	0	0
03	0	0	0	0
04	0	0	0	0
05	0	0	0	0
06	0	0	0	0
07	0	0	0	0
08	0	0	0	0
09	0	0	0	0
10	0	0	0	0
11	0	0	0	0
12	0	0	0	0
13	0	0	0	0
14	0	0	0	0
15	0	0	0	0
16	0	0	0	0
17	0	0	0	0
18	0	0	0	0
19	0	0	0	0
20	0	0	0	0

Min	0	15	30	45
21	0	0	0	0
22	0	0	0	0
23	0	0	0	0
24	0	0	0	0
25	0	0	0	0
26	0	0	0	0
27	0	0	0	0
28	0	0	0	0
29	0	0	0	0
30	0	0	0	0
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32	0	0	0	0
33	0	0	0	0
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35	0	0	0	0
36	0	0	0	0
37	0	0	0	0
38	0	0	0	0
39	0	0	0	0
40	0	0	0	0

Min	0	15	30	45
41	0	0	0	0
42	0	0	0	0
43	0	0	0	0
44	0	0	0	0
45	0	0	0	0
46	0	0	0	0
47	0	0	0	0
48	0	0	0	0
49	0	0	0	0
50	0	0	0	0
51	0	0	0	0
52	0	0	0	0
53	0	0	0	0
54	0	0	0	0
55	0	0	0	0
56	0	0	0	0
57	0	0	0	0
58	0	0	0	0
59	0	0	0	0
60	0	0	0	0

NOTES: NO VISIBLE EMISSIONS

Inspector R. X. Skinner Date 7-26-79

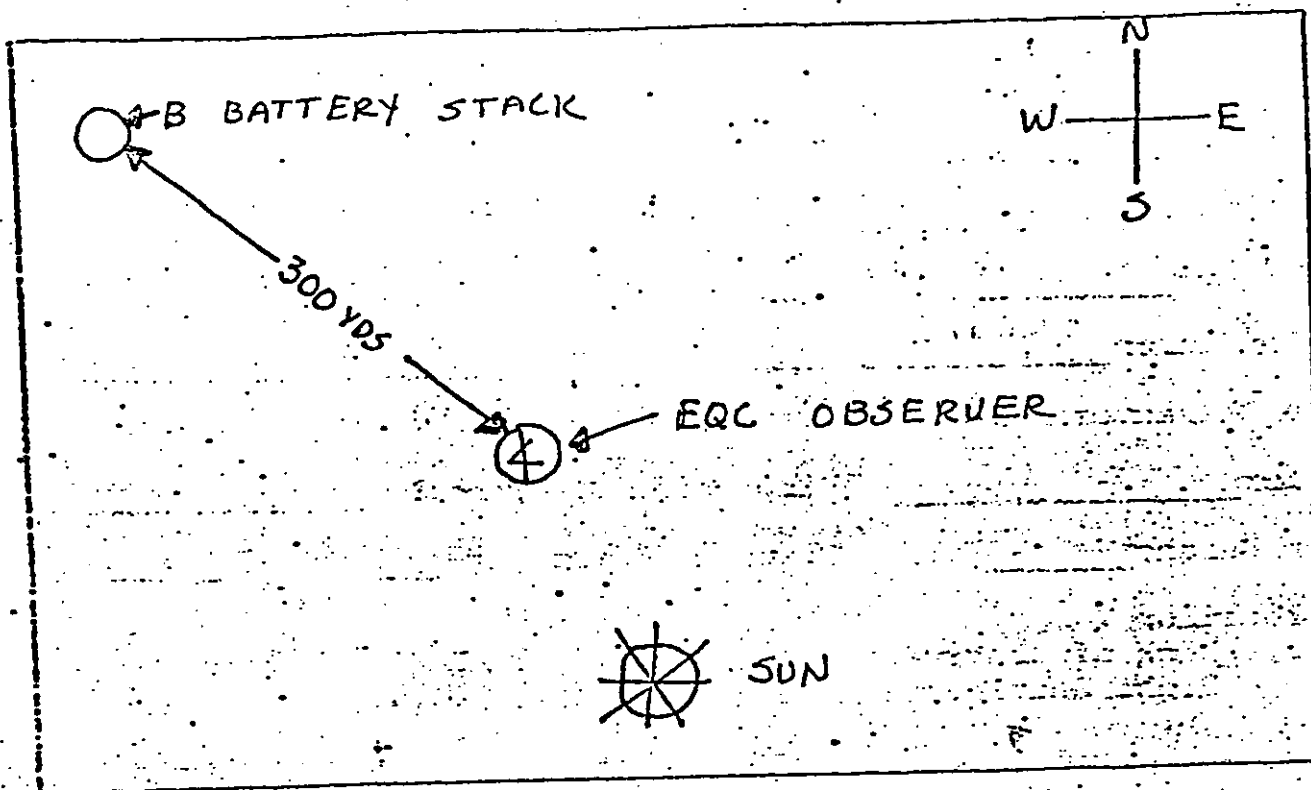
TSB-A-8

EPA-IX-FORM 208

ABOVE INSPECTOR CERTIFIED BY C.A.R.S.
 ON 5-10-79

MAP

1140 1240



Symbols

Sun = ☼

Plume direction = —→

Water Vapor Condensate

Point where plume observed =

Observer = 4

Photographs: S&A File ()

Enclosed ()

None ()

Comments

Signature

R. L. Ripper

Date

7-27-79

VISIBLE EMISSION OBSERVATION RECORD

Company KAISER STEEL CORP

Date 27 July 79

Time First Sighted Plume _____

Time Start 0925

Time Stop 1025

Air Temperature 77°

Relative Humidity _____

Wind Speed 3-5 MPH

Wind Direction SSW

Sky Condition CLEAR WAZE

Background SUN

Plume Characteristics:

Continuous: () yes (X) no

Dispersion Description _____

Color _____

Stack Height 125 (ft)

Observer location: 975 (ft) SW of stack

Sun location

() Back of Observer
(X) Right Shoulder

() Left Shoulder
() Other

Emission Point B BATTERY CASE AVEN STACK

Min	0	15	30	45
01	☉	☉	☉	☉
02	☉	☉	☉	☉
03	☉	☉	☉	☉
04	☉	☉	☉	☉
05	☉	☉	☉	☉
06	☉	☉	☉	☉
07	☉	☉	☉	☉
08	☉	☉	☉	☉
09	☉	☉	☉	☉
10	☉	☉	☉	☉
11	☉	☉	☉	☉
12	☉	☉	☉	☉
13	☉	☉	☉	☉
14	☉	☉	☉	☉
15	☉	☉	☉	☉
16	☉	☉	☉	☉
17	☉	☉	☉	☉
18	☉	☉	☉	☉
19	☉	☉	☉	☉
20	☉	☉	☉	☉

Min	0	15	30	45
21	☉	☉	☉	☉
22	☉	☉	☉	☉
23	☉	☉	☉	☉
24	☉	☉	☉	☉
25	☉	☉	☉	☉
26	☉	☉	☉	☉
27	☉	☉	☉	☉
28	☉	☉	☉	☉
29	☉	☉	☉	☉
30	☉	☉	☉	☉
31	☉	☉	☉	☉
32	☉	☉	☉	☉
33	☉	☉	☉	☉
34	☉	☉	☉	☉
35	☉	☉	☉	☉
36	☉	☉	☉	☉
37	☉	☉	☉	☉
38	☉	☉	☉	☉
39	☉	☉	☉	☉
40	☉	☉	☉	☉

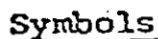
Min	0	15	30	45
41	☉	☉	☉	☉
42	☉	☉	☉	☉
43	☉	☉	☉	☉
44	☉	☉	☉	☉
45	☉	☉	☉	☉
46	☉	☉	☉	☉
47	☉	☉	☉	☉
48	☉	☉	☉	☉
49	☉	☉	☉	☉
50	☉	☉	☉	☉
51	☉	☉	☉	☉
52	☉	☉	☉	☉
53	☉	☉	☉	☉
54	☉	☉	☉	☉
55	☉	☉	☉	☉
56	☉	☉	☉	☉
57	☉	☉	☉	☉
58	☉	☉	☉	☉
59	☉	☉	☉	☉
60	☉	☉	☉	☉

NOTES: _____

Inspector R. Bann

Date 7/27/79

C925-1025



Sun = ☉

Plume direction = $\rightarrow$

Point where plume observed =

Observer = 4

Water Vapor Condensate

Photographs: S&A File ()

Enclosed (2)

None ()

Comments

Signature

Robert B. Beair

Date _____

7/27/79

VISIBLE EMISSION OBSERVATION RECORD

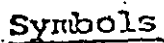
Company KAISER STEEL CORP Run 2
 Date 7/27/79 Time First Sighted Plume _____
 Time Start 1140 Time Stop 1240
 Air Temperature 90°F Relative Humidity _____
 Wind Speed 8-11 MPH Wind Direction SW
 Sky Condition CLEAR - HAZE Background sky
 Plume Characteristics: Continuous: () yes (☒) no
 Color NA Dispersion Description NA
 Stack Height 125 (ft) Observer location: 975 (ft) SE of stack
 Sun location (☒) Back of Observer () Left Shoulder
 () Right Shoulder () Other
 Emission Point BATTERY COKE OVEN STACK

Min	0	15	30	45
01	☉	☉	☉	☉
02	☉	☉	☉	☉
03	☉	☉	☉	☉
04	☉	☉	☉	☉
05	☉	☉	☉	☉
06	☉	☉	☉	☉
07	☉	☉	☉	☉
08	☉	☉	☉	☉
09	☉	☉	☉	☉
10	☉	☉	☉	☉
11	☉	☉	☉	☉
12	☉	☉	☉	☉
13	☉	☉	☉	☉
14	☉	☉	☉	☉
15	☉	☉	☉	☉
16	☉	☉	☉	☉
17	☉	☉	☉	☉
18	☉	☉	☉	☉
19	☉	☉	☉	☉
20	☉	☉	☉	☉

Min	0	15	30	45
21	☉	☉	☉	☉
22	☉	☉	☉	☉
23	☉	☉	☉	☉
24	☉	☉	☉	☉
25	☉	☉	☉	☉
26	☉	☉	☉	☉
27	☉	☉	☉	☉
28	☉	☉	☉	☉
29	☉	☉	☉	☉
30	☉	☉	☉	☉
31	☉	☉	☉	☉
32	☉	☉	☉	☉
33	☉	☉	☉	☉
34	☉	☉	☉	☉
35	☉	☉	☉	☉
36	☉	☉	☉	☉
37	☉	☉	☉	☉
38	☉	☉	☉	☉
39	☉	☉	☉	☉
40	☉	☉	☉	☉

Min	0	15	30	45
41	☉	☉	☉	☉
42	☉	☉	☉	☉
43	☉	☉	☉	☉
44	☉	☉	☉	☉
45	☉	☉	☉	☉
46	☉	☉	☉	☉
47	☉	☉	☉	☉
48	☉	☉	☉	☉
49	☉	☉	☉	☉
50	☉	☉	☉	☉
51	☉	☉	☉	☉
52	☉	☉	☉	☉
53	☉	☉	☉	☉
54	☉	☉	☉	☉
55	☉	☉	☉	☉
56	☉	☉	☉	☉
57	☉	☉	☉	☉
58	☉	☉	☉	☉
59	☉	☉	☉	☉
60	☉	☉	☉	☉

NOTES: OBSERVATIONS MADE WITH EYE AND BINOCULARS -
IF THERE WERE EMISSIONS FROM A BATTERY STACK
THEY WERE LESS THAN 5% opacity AND NOT VISIBLE FROM
my location
 Inspector Robert B. Bean Date 27 July 79



Point where plume observed =
Observer = 4

Water Vapor Condensate

Photographs: S&A File () Enclosed () None ()

Comments

Signature

Robert B Brain

Date _____

7/27/27

7/27/79 FRIDAY

"B" STACK BAGHOUSE

compartments						Total ΔP	INLET TEMP.	o/o Opacity	INSTRUMENT	NOT ON LINE	CONTRACTOR HAS NOT
2	1	2	3	4	5						
25	7.15	6.70	6.50	8.10	5.95	6.20	450	SATISFIED	Operation/Calibration	Contract	Specs.
30	7.15	6.75	6.50	8.15	5.95	6.20	450				
35	7.15	6.75	6.50	8.15	6.00	6.00	450				
40	7.15	6.80	6.50	8.15	6.05	6.30	450				
45	7.20	6.80	6.50	8.20	6.05	6.50	450				
50	7.25	6.85	6.60	8.25	6.15	6.50	450	Operation/Calibration	Contract	Specs.	CONTRACTOR HAS NOT
55		6.85	6.60	8.25	6.05	8.00	450				
60		6.90	6.65	8.25	6.20	6.50	450				
65		6.85	6.65	8.25	6.20	6.40	455				
70		6.95	6.70	8.35	6.20	6.40	455				
75		6.85	6.60	8.25	6.15	6.40	450	Operation/Calibration	Contract	Specs.	CONTRACTOR HAS NOT
80		6.85	6.55	8.20	6.15	6.40	455				
85		6.85	6.60	8.25	6.15	6.40	455				
90						ave.	ave.				
95						6.43	452				

H 0955 Disconnected #1 Compartment
 Manometer - All Readings from then
 until 1025 ~~are~~ are with 1 off.

Charge 84 @ 0928 - Charge 56 @ 1020
 Push 56 @ 1010 - Push 66 @ 1019

"B" STACK BAGHOUSE

7/27/79

FRIDAY

2	1	compartments				6	Total ΔP	INLET TEMP.	o/o Opacity	INSTRUMENT OPERATION / CALIBRATION	NOT ON LINE CONTRACTOR SPECS.
		2	3	4	5						
35		7.15	6.75	8.45	6.30		7.00	465			
40		7.20	6.75	8.50	6.35		7.00	465			
45		7.20	6.80	8.50	6.35		7.00	465			
50		7.20	6.80	8.55	6.35		7.00	465			
55		7.20	6.80	8.50	6.35		6.90	465			
60		7.15	6.80	8.45	6.35		6.90	465			
65		7.15	6.80	8.45	6.35		6.90	465			
70		7.25	6.80	8.50	6.35		7.00	465			
75		7.25	6.80	8.55	6.45		6.90	465			
80		7.25	6.80	8.55	6.45		6.90	465			
85		7.25	6.80	8.55	6.45		7.00	465			
90		7.25	6.80	8.60	6.45		7.00	465			
95		7.25	6.80	8.60	6.45		7.00	465			
							ave =	ave =			
							6.96	465			

#1 Compartment Manometer Still Off.

Push 53 @ 1133 - Push 72 @ 1146
 Charge 58 @ 1148 - Charge 78 @ 1155

SOTDAT/STEEL LIBRARY SYSTEM

Report Title:

Plant and Location: Kaiser Steel Fontana, CA

SCC: 30300306

Testing Date(s): 7/26-27/79

By Whom: company

Stack Test Review Attached:

Reviewed by:

Problems Seen by Reviewer:

Confidentiality Status: Clear

If status is confidential, list confidential pages or sections:

Source of Determination of the Confidentiality Status: Memo entitled:
"Steel Technical Support Materials" From: Edward Reich,
Director DSSE, To: Tom Voltaggio

Report Encoded by:

Date Encoded:

Form Numbers:

Comments:

Title: *see title page*

Plant and Location: *Kaiser Steel, Fontana, CA*

SCC: *30 300306*

Test Date: *7/26-27/79*

By Whom: *Company*

Encoded By:

Date Encoded:

Completed By:

Form No.:



U.S.E.P.A.
REGION IX
COMM CONTR

ENGINEERING-SCIENCE

125 WEST HUNTINGTON DRIVE • P.O. BOX 538 • ARCADIA, CALIFORNIA 91006 213/445-7560

CABLE ADDRESS: ENGINSKI
TELEX: 67-5426

3126.00

20 August 1979

Mr. Gary Lavagnino
Task Manager (S-2-1)
Surveillance and Analysis Division
U.S. Environmental Protection Agency
Region IX
215 Fremont Street
San Francisco, CA 94105

Dear Mr. Lavagnino:

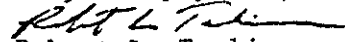
Attached is a report on observations made during a series of source tests conducted at Kaiser Steel Corporation, Fontana, California on July 26-27, 1979. These tests were to determine particulate emissions from a baghouse controlling stack gases in the battery B coke ovens.

The tests were conducted by the Environmental Quality Control Section of Kaiser Steel Corporation, pursuant to Paragraph X of the Amended Consent Decree entered on September 30, 1977, Case No. CV 76-0675MML (U.S. District Court, Central District of California).

Four EPA Method 5 tests were conducted of which the first two tests were discarded due to pitot tube error. Water was found in the pitot tube lines, causing incorrect pitot tube readings.

The source test results and visual opacity observations of July 26-27, 1979 indicate compliance of the baghouse emissions with Rules 409A and 405A of the South Coast Air Quality Management District.

Very truly yours,


Robert L. Tomlinson
Environmental Engineer

RLT:he
Enclosures

cc: J. R. Busik
S. J. Hitte
E. McLean
L. Genoble (ES)



ENGINEERING-SCIENCE

125 WEST HUNTINGTON DRIVE • P.O. BOX 538 • ARCADIA, CALIFORNIA 91006 • 213/445-7560

CABLE ADDRESS: ENGINS
TELEX: 67-5428

12 September 1979

Mr. Gary Lavagnino, Task Manager
Surveillance & Analysis Division
U.S. EPA, Region IX
215 Fremont Street
San Francisco, CA 94105

Dear Mr. Lavagnino:

The following information is submitted in answer to your August 30, 1979 questions regarding the Kaiser Steel Battery B source test observation and the Firestone Tire Company and Seaside Paint and Lacquer Company SIP inspection reports.

- (1) The Kaiser Steel source test team was not equipped to conduct a 90° traverse without considerable effort and possible sampling train breakdown problems. The only probe available for the test was 10 feet long, and without a monorail for support, the heavy probe would have been difficult to hand-hold for a 30-minute traverse. The SCAQMD agreed with Kaiser Steel that two horizontal traverses conducted one immediately after the other would be sufficient for the EPA Method 5 test.
- (2) Several of the source tested Battery B coke ovens were being repaired or relined with bricks during the test. The result of these repairs was a process weight of 37,000 lbs./hr. instead of the typical 60,000-70,000 lbs./hr.
- (3) Specific design data for the Battery B baghouse will be available from Kaiser Steel on September 13, 1979 during the inspector's visit to the plant for cast house visible emission observations. The information will then be forwarded to your office.
- (4) Attached is a copy of SCAQMD Rule 462 which regulates the operation of organic liquid loading facilities. The Firestone Tire Company and Seaside Paint and Lacquer Company organic liquid storage tanks are all under the Rule 462 applicable size of 20,000 gallons. No other rules in the SCAQMD regulations appear to require submerged fill pipes for such organic liquid storage tanks.

Very truly yours,

Robert L. Tomlinson
Environmental Engineer

RLT:eh
Attachment



ENGINEERING-SCIENCE

125 WEST HUNTINGTON DRIVE • P.O. BOX 538 • ARCADIA, CALIFORNIA 91006 • 213/445-7560

CABLE ADDRESS: ENGINS
TELEX: 67-5428

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SEP 21 11 27 AM '79

18 September 1979

Mr. Gary Lavagnino
Task Manager (S-2-1)
Surveillance & Analysis Division
EPA Region IX
215 Fremont Street
San Francisco, CA 94105

Subject: Requested information for the
Kaiser Steel Battery B Coke Oven Baghouse

Dear Mr. Lavagnino:

The baghouse utilized by Kaiser Steel to control emissions from the Battery B coke ovens is an American Air Filter Type 8, size 5-180 continuous automatic suction dust collector. Five collector modules for the system are arranged back to back in two rows of five modules. The collector utilizes a common reverse air system with the Battery C baghouse. Design air/cloth ratio is approximately 1.5:1.

Attached are copies of the correspondence between the SCAQMD and Kaiser Steel that documents the District's approval of Kaiser Steel's source test method for the Battery B baghouse.

Very truly yours,

Robert L. Tomlinson
Environmental Engineer

RLT:eh

Enclosure

bcc:

J. D. Carlson
W. P. Smith
R. E. Garner, FO
A. M. Kashay, FO
R. E. Robinson, FO
G. L. Rounds, FO
H. M. Smith, FO
R. D. Wight, FO
D. W. Jordan, Sr., Esq.,
San Bernardino

June 20, 1979

Certified Mail - Return Receipt Requested

U. S. Environmental Protection Agency
Region IX
215 Fremont Street
San Francisco, California 94105

Attention: Director, Enforcement Division

Gentlemen:

As discussed by Mr. H. M. Smith with Ms. Lois Green of your staff, this confirms that intended testing of "B" Battery stack has been changed to July 26 and 27, 1979 from June 26 and 27 as notified in our letter of May 25, 1979. Your accommodation to this change is greatly appreciated.

Very truly yours,

KAISER STEEL CORPORATION

By James E. Good
Attorney for Defendant

JEG:lf

cc: Mr. Thomas Austin, ARB
Mr. C. A. O'Malley, Eastern Zone, SCAQMD
Mr. L. Stiles, Eastern Zone, SCAQMD





South Coast
AIR QUALITY MANAGEMENT DISTRICT

EASTERN ZONE
22850 COOLEY DRIVE, COLTON, CALIFORNIA 92323 (714) 824-2660

April 20, 1979

Mr. G. L. Rounds, Director
Environmental Quality Control
Steel Manufacturing Division
Kaiser Steel Corporation
P. O. Box 217
Fontana, CA 92335

Dear Mr. Rounds:

REF: Your letter of April 19, 1979, "KSC Coke Plant Battery "B"
Stack Compliance Tests"

The District has no objection to sampling the horizontal diameter, only, as described in subject letter on Coke Ovens Battery "B" Baghouse compliance tests. In all other matters, we expect you to follow the South Coast Air Quality Management District "Source Testing Manual", Second Printing, August, 1978.

You are reminded that SCAQMD source testing procedures, regarding particulates collection, are more strict than EPA Method 5, and you are expected to follow them.

We await your 30 day advance notification of the firm testing dates, and, as usual, we will provide a qualified source test observer.

Very truly yours,

Robert J. MacKnight
Director of Engineering

Charles A. O'Malley

Charles A. O'Malley
Chief Engineer, Colton Office



CAD:esg

cc: EPA, Region IX, Director of Enforcement,
Clyde B. Eller

**KAISER
STEEL**

KAISER STEEL CORPORATION
STEEL MANUFACTURING DIVISION
P. O. BOX 217 W. FONTANA, CA 92335

April 18, 1979

Mr. Charles A. O'Malley
Chief Engineer, Colton Office
South Coast Air Quality Management District
22850 Cooley Drive
Colton, California
92324

Subject: KSC Coke Plant Battery "B" Stack
Compliance Tests.

Ref: Amended EPA Consent Decree No CV 76-0675 MML.
Pages 1-5 incl.

Dear Mr. O'Malley:

We are required by section IVB, 5, C, of the reference to demonstrate compliance with SCAQMD Rule 50A (opacity) by August 1, 1979 for coke battery "B" stack. In addition to demonstrating compliance with Rule 50A we will also demonstrate compliance with Rules 404(a), and 405(a) as we have done for Coke Battery Stacks "C", "D", and "E".

The baghouse exit sampling locations for batteries C, D, and E, were all in the vertical duct immediately prior to the exhaust fan. Sampling equipment used for demonstration of compliance with Rules 404(a) and 405(a) was a GII (Glass Innovators Inc.) super probe 8' long with an EPA 5 type sampling train. The baghouse exit sampling location on "B" Battery is in a long run of 61" ID horizontal duct.

We will not be able to use our GII EPA 5 sampling train on "B" battery baghouse if we are required to sample the horizontal duct on two diameters as specified in EPA Method 5. We, therefore, request your concurrence in sampling only the horizontal diameter with the GII sampling train. The sampling location has approximately 12 unobstructed pipe diameters upstream and 4 diameters downstream. We feel that sampling the horizontal diameter only would yield a valid sample. Of course, velocity profiles will be determined on both horizontal and vertical planes.

The sample dates for compliance testing of "B" battery baghouse are tentatively set for June 26 and 27, 1979. Please advise us of your thoughts about sampling the horizontal plane only. We will notify you 30 days in advance of firm testing dates.

Sincerely yours,

G. L. Rounds
G. L. Rounds, Director
Envir. Quality Control