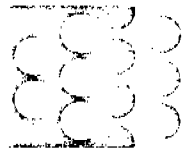


Note: This is a reference cited in AP 42, *Compilation of Air Pollutant Emission Factors, Volume I Stationary Point and Area Sources*. AP42 is located on the EPA web site at www.epa.gov/ttn/chief/ap42/

The file name refers to the reference number, the AP42 chapter and section. The file name "ref02_c01s02.pdf" would mean the reference is from AP42 chapter 1 section 2. The reference may be from a previous version of the section and no longer cited. The primary source should always be checked.

Compliance Tests of the
Envirotech Hooded Quench Car No. 104
Operated on the
Number 20 Coke Battery
Located at the
United States Steel Clairton Works



File No. 50.50
2/12/85

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Envirotech Hooded Quench Car No. 104
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VOLUME I - Test Report

Clairton, PA 15025

Project No. 50.50

February 12, 1985

Prepared by:
Dr. R.G. Patterson



AIR POLLUTION
TECHNOLOGY, INC.

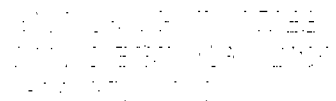


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Compliance Tests of the
Envirotech Hooded Quench Car No. 104
Operated on the
Number 20 Coke Battery
Located at the
United States Steel Clairton Works

INTRODUCTION

This report covers test work performed by Air Pollution Technology, Inc. (APT) in cooperation with United States Steel Corporation (USSC) and Envirotech Corporation (EVT) on the Envirotech Hooded Quench Car No. 104 (HQC) operating on the No. 20 coke batteries located at the USSC's Clairton Cokeworks. The purposes of these tests were to measure the particulate and visible emissions from the HQC.

The EVT HQC system is designed to capture and remove particulates from the hot gases during coke-pushing operations. The basic HQC System consists of three major components.

1. A self propelled Control Car, which houses all induced draft and gas cleaning equipment. This car carries the Aeronetics Hot Water Scrubber that provides both the draft required to capture the gases at the system inlet and the fine water drops required to collect particulates in the gas stream during the scrubbing process.
2. A One-Spot Hooded Quench Car, which consists of a tilting coke box covered by a fixed hood to contain the gases so that they can be drawn into and through the control car for cleaning. The hood encloses the quench car on three sides and the top, with the side facing the ovens open to receive the coke pushed.
3. Minor modifications, as required, to the existing coke guide to prevent gases from escaping to the atmosphere during the coke push. Wings are added to the face of the coke guide on both sides of the coke discharge opening. The wings align with the open face of the quench car hood when the car is positioned for the push.

The Aeronetics hot water scrubber, considered the "heart" of the system, incorporates a two-phase adjustable jet nozzle in

which water is ejected to perform the dual functions of gas movement and gas scrubbing. The water/vapor combination in the scrubber is referred to as a two-phase phenomenon.

The Aeronetics scrubber directs pressurized hot water to provide the energy for moving large quantities of gas through the scrubbing system. The nozzle's jet ejector effect transfers momentum from the liquid to the gas. Additionally, the jet nozzle atomizes the liquid and accelerates it to velocities of more than 1,000 feet per second, thereby creating a large velocity differential between the drops and the suspended particles in the gas stream. This relative velocity causes inertial impaction between the drops and the particles. As inertial impaction occurs, the particles are deposited on the drops, which are then removed from the gas stream by means of an entrainment separator. The cleaned gas exits into the atmosphere and the particulated liquid flows into a drain.

Recently, EVT made several modifications to the basic HQC system to improve the particle collection efficiency. They are as follows:

1. The effectiveness of the quench car hood was increased by extending the transition duct into the hood so as to cause more symmetrical gas flow within the hood. This increases the efficiency of fugitive emissions capture.
2. The collection efficiency was increased by pre-conditioning the gas prior to entering the Aeronetics scrubbers by spraying water into the gas stream. This increases the liquid to gas (L/G) ratio in the scrubber throat.

The particle mass concentration was measured at the outlet of the HQC with an EPA Method 5 sampling train. The visible emissions observations were done simultaneously with the particulate mass concentration measurements at the request of the Allegheny County Health Department Bureau of Air Pollution Control (BOAPC). The compliance test results presented in this report are for tests completed on December 5, 6, 13 and 14, 1984. Pre-compliance tests completed on October 19, 21, 23 and 24 which were run under similar operating conditions are also presented in this report at the request of the BOAPC. All tests were completed while the car was receiving and transporting coke from the Number 20 coke battery.

SUMMARY

The following points summarize the results of the compliance tests completed on the EVT Hooded Quench Car No. 104. Three compliance tests were conducted during normal coking conditions.

3. Compliance test protocol presented in Appendix F complies with the USSC consent decree, as modified, for coke pushing emissions and has been approved by the Allegheny County Health Department, Bureau of Air Pollution Control, Pennsylvania Department of Environmental Resources and the Environmental Protection Agency.

Battery 20 is considered a new source and is subject to the Lowest Achievable Emission Rate (LAER) standard. Pursuant to the Consent Decree, as modified, the applicable LAER emissions standards for particulates, and as discussed with the regulatory agencies, are as follow:

1. Particulate mass emission less than or equal to 0.04 pounds per ton of coke pushed.
2. Visible emissions during push and travel less than 20 percent.
3. USSC has been informed by BOAPC, as shown in Appendix G, that opacity standards during travel should be less than 20% since USSC uses pushing emission control devices.

APPROACH

1. Carry out particulate mass and visible emission measurements on the HQC system. This involved the following:
 - a. Two of the test personnel were on the test car to operate the particulate mass emission sampling apparatus. One of the personnel operated the sampling train control module. The other person measured the gas velocity head and converted that number into a sample train flowrate for the sample train operator. This helped the sample train operator maintain isokinetic sampling conditions. The second person also signaled the start, stop and change from push to travel modes for the sample train operator.
 - b. One test person was assigned to measure the visible emissions from the HQC system during the push and travel cycles.
 - c. One test person was assigned to ride in the cab of the HQC control car to record the car operating parameters.
 - d. All process operating data were supplied by the Clairton Cokeworks Operations personnel.
2. Analyze all samples in a field lab set up in a construction trailer at the test site. The analyses were completed by the sample crew leader.
3. Reduce and analyze the test data.

4. Determine the particulate and visible emission performance of the HQC and compare these results with the LAER emission standards.

TEST PERSONNEL AND OBSERVERS

Following is a list of test personnel and observers:

Field Test Personnel:

- Dr. Ronald G. Patterson, Project Engineer
- Mr. Bruce C. DaRos, Field Test Crew Leader
- Mr. Paul Jarman, Sampling Train Operator
- Mr. Sherman Smith, Pitot Tube Operator
- Mr. Cary Milburn, Pitot Tube Operator
- Ms. Linda Lancaster, Visible Emissions Observer

Allegheny County Board of Air Pollution Control Observers:

- Mr. K. Shankar N. Banninathaya, Air Pollution Engineer
- Mr. William J. Logan, Air Pollution Control Technician
- Mr. Thomas Kelly, Coke Oven Technician
- Mr. Clarence Carey, Coke Oven Technician

USSC Personnel:

- Mr. Joseph Connelly, Project Engineer
- Mr. Larry Gainer, Division Superintendent, Gas & Coke
- Mr. Roy Weiskircher, Senior Environmental Engineer
- Mr. Randy York, Environmental Consultant
- Mr. Michael J. McKelvey, Field Construction Manager
- Mr. Robert Brown, BCM Visible Emissions Observer

EVT Personnel:

- Mr. Patrick J. Reilly, Vice President and Project Manager
- Mr. Ned H. Ford, Field Construction Manager
- Mr. Ira Lapof, Field Construction Superintendent
- Mr. Frank Kress, Control Car Operations

Consultants to EVT:

- Dr. Seymour Calvert, Environmental Engineering and Testing Consultant
- Mr. Frank Lauer, Coking Consultant

TEST SITE AND OPERATING CONDITIONS

Metallurgical grade coke is produced by USSC at the Clairton Works by heating coal in an inert atmosphere at approximately 2,600°F for a period of 18 to 21 hours to drive off volatile compounds and impurities, such as sulfur.

Each coke battery consists of a number of ovens which are charged from the top with a coal mixture. The coal mixture is heated by circulating hot gas through flues which form the

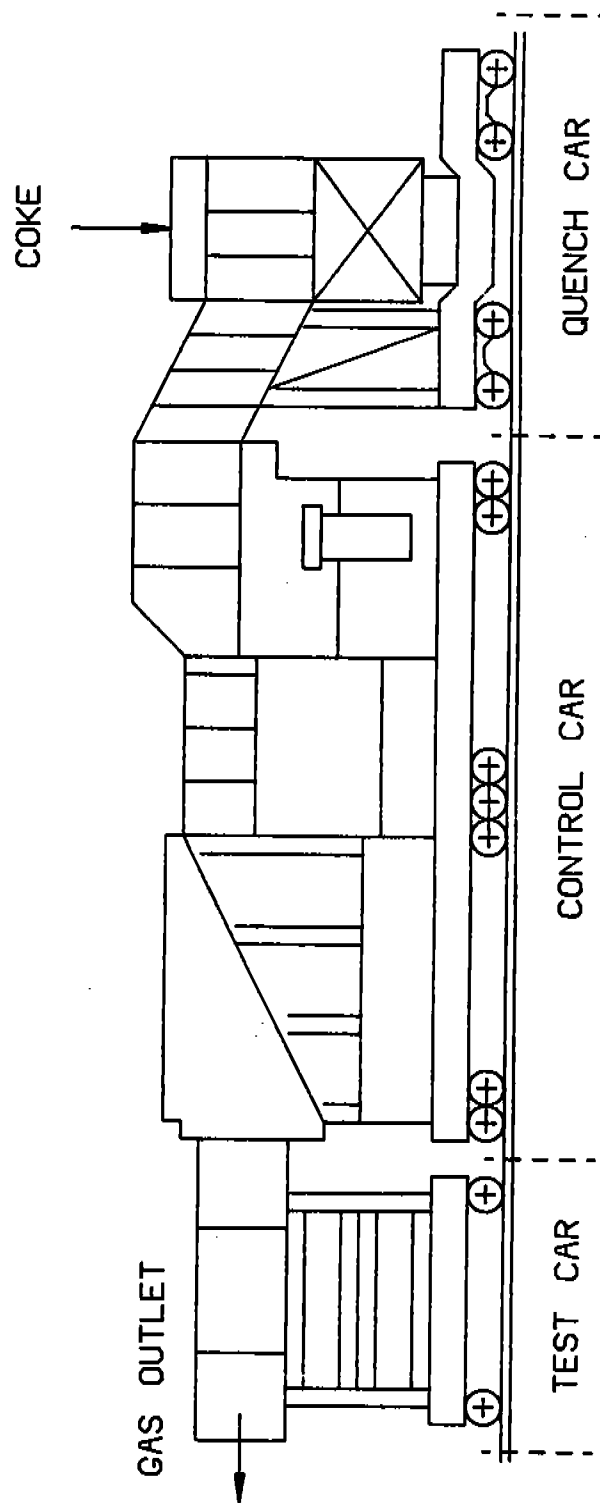


Figure 1. Envirotech Hooded Coke Quench Car System.

deposited on the drops, which are then removed from the gas stream by means of an entrainment separator. The cleaned gas exits into the atmosphere and the particulated liquid flows into a drain.

Recently, EVT made several modifications to the basic HQC system to improve the particle collection efficiency. They are as follow:

1. The effectiveness of the quench car hood was increased by extending the transition duct into the hood so as to cause more symmetrical gas flow within the hood. This increases the efficiency of fugitive emissions capture.
2. The collection efficiency was increased by pre-conditioning the gas prior to entering the Aronetics scrubbers by spraying water into the gas stream. This increases the liquid to gas (L/G) ratio in the scrubber throat.

Process condition data for the HQC System were recorded for each traverse point as shown in Appendix A. Tables 1 and 2 show the average data for the HQC system for each of the compliance and pre-compliance tests. During both of these test series the average production rate for coke battery number 20 was 14.5 tons of coke per oven.

TESTS RESULTS

A number of pre-compliance tests were run with the HQC System under different operating conditions and combinations of modifications. The results from the pre-compliance tests run on the HQC System as described on page 1, as well as the compliance tests are presented in this section:

Test Number	Date	Test Type	Coking Conditions
3.1	10/19/84	Pre-comp.	Normal
3.2	10/21/84	"	"
3.3	10/23/84	"	"
3.4	10/24/84	"	"
7.1	12/5/84	Compliance	"
7.2	12/6/84	"	Upset
7.4	12/13/84	"	Normal
7.5	12/14/84	"	"

Test number 7.2 was completed during upset operating conditions on the number 20 battery. The pusher machine was out for fourteen hours during the previous night's turn, which upset the normal pushing schedule. Test number 7.3 was started on December 7, 1984, but was aborted because of the low ambient

**TABLE 1. AVERAGE HQC SYSTEM PROCESS CONDITION DATA
COMPLIANCE TESTS**

Test Number	7.1		7.2		7.4		7.5	
	Push	Travel	Push	Travel	Push	Travel	Push	Travel
Nozzle Water Flowrate, gpm	351	115	350	115	365	115	361	119
Water Temp, deg F*	429	429	429	429	414	414	414	414
Water Press, psig	294	287	295	287	295	286	294	286
Annubar Vel Head, in. WC	3.0	1.0	3.0	1.0	3.1	1.5	3.1	1.4
Scrubber Temp In, deg F**	145	132	145	131	200	174	197	171
Scrubber Temp Out, deg F	156	158	161	164	160	161	158	159
Pre-spray H ₂ O Flowrate, gpm***	400	0	400	0	400	0	400	0

* Water temperature reported here was the tank temperature.

** The inlet scrubber gas temperature thermocouple was recalibrated prior to test number 7.4.

***The quench water flowrate was assumed to be 400 gpm from the pump specifications.

TABLE 2. AVERAGE HQC SYSTEM PROCESS CONDITION DATA
PRE-COMPLIANCE TESTS

Test Number	3.1		3.2		3.3		3.4	
	Push	Travel	Push	Travel	Push	Travel	Push	Travel
Nozzle Water Flowrate, gpm	401	110	397	110	382	110	373	110
Water Temp, deg F	419	418	425	423	417	417	424	424
Water Press, psig	299	288	305	296	297	287	295	286
Annubar Vel Head, in. WC	2.0	0.9	2.9	1.3	0.0	0.0	2.6	1.3
Scrubber Temp In, deg F***	142	166	142	144	148	142	165	147
Scrubber Temp Out, deg F	154	158	156	159	155	159	155	161
Pre-spray H ₂ O Flowrate, gpm*	400	0	400	0	400	0	400	0

* The quench water flowrate was assumed to be 400 gpm from the pump specifications.

** See notes regarding thermocouple calibration on Table 1.

temperature. The ambient temperature was approximately 10°F and the impinger outlet temperature was 15°F which indicated that the impinger water could have frozen during the test.

Tables 3 and 4 are summaries of the test conditions for each of the tests. Tables 5 through 7 and 8 through 10 show the particulate emission results for the compliance and the pre-compliance tests. Tables 5 and 8 compare the particulate emission rate in lb/ton of coke pushed to the EAER emission standard for each of the tests. The results of the visible emission observations are summarized in Table 11.

TEST METHODS

The tests results presented in this report were completed according to the Compliance Test Protocol shown in Appendix F. The particulate emission tests were completed with the Method 5 particulate emission sampling system modified as approved for these tests, as shown in Figure 2. The probe, cyclone and filter holder were Teflon lined or coated. Two impinger trains were used in parallel to accommodate the high sample flowrate required to collect a sample volume greater than 30 dscf.

The 24 sampling locations are shown in Figure 3. A cyclonic flow test completed on November 21, 1984 showed an average cyclonic flow angle of 1.8 degrees for all points during push and travel. The results of the cyclonic flow test are shown in Appendix I. All sample analysis was completed in a field laboratory set up in a construction trailer near the test site.

All fugitive visible emission observations were completed simultaneously with the particulate emission tests. The test car was attached during the visible emission observations. This increased the pressure drop that the Aeronetics nozzle had to overcome, which decreased the gas flowrate and the ability of the HQC System to capture fugitive emissions during these tests.

TABLE 3. SUMMARY OF COMPLIANCE TEST CONDITIONS

Test Number	7.1		7.2		7.4		7.5	
	Push	Travel	Push	Travel	Push	Travel	Push	Travel
Avg Gas Vel, fps	67.4	34.3	66.5	34.6	69.2	38.9	66.2	36.2
Avg Gas Flow rate, acfm	129968	66069	128130	66652	133306	75021	127571	69697
Avg Gas Flow rate, dscfm	76222	38653	68609	35520	74808	42034	73539	40124
Exit Gas, deg F	156	158	161	164	160	161	158	159
Exit Press, in. Hg	29.41	29.41	28.99	28.99	29.23	29.23	29.49	29.49
Samp. Vol., dscf (corr.)	22.26	11.14	19.92	11.31	21.12	13.51	20.26	12.99
% Isokinetic	109	105	103	105	101	112	101	102
	Total		Total		Total		Total	
Samp. Vol., dscf (corr.)	33.40		31.24		34.64		33.25	
Dry Gas Comp.								
CO ₂ (vol %)	2.0		2.2		2.1		2.1	
O ₂ (vol %)	18.2		17.3		18.3		18.3	
CO (vol %)	0.2		0.3		0.0		0.0	
N ₂ (vol %)	79.6		80.2		79.7		79.7	
Moisture, vol%								
M-5	30.38		37.47		32.60		33.85	
Sat. at T out	30.44		35.04		33.02		31.54	
Mol Wt,								
Dry	29.05		29.04		29.06		29.06	
Wet	25.69		25.17		25.45		25.57	
Front-half Part., mg	34.77		79.77		45.73		30.08	
Back-half Part., mg	1.40		2.09		1.69		1.46	
Total DER Part, mg	36.17		81.86		47.42		31.54	

TABLE 4. SUMMARY OF PRE-COMPLIANCE TEST CONDITIONS

Test Number	3.1		3.2		3..3		3.4	
	Push	Travel	Push	Travel	Push	Travel	Push	Travel
Avg Gas Vel, fps	74.6	41.5	68.9	40.2	66.4	35.3	62.9	36.5
Avg Gas Flow rate, acfm	143837	79949	132752	77491	127908	68038	121298	70390
Avg Gas Flow rate, dscfm	89946	49714	80884	46960	80079	42308	78584	45212
Exit Gas, deg F	154	158	156	159	155	159	155	161
Exit Gas, in. Hg	30.486	30.486	30.373	30.373	30.763	30.763	30.753	30.753
Samp. Vol., dscf (corr.)	24.33	15.36	12.72	6.60	23.40	13.92	24.57	11.46
% Isokinetic	90	107	98	99	99	112	107	91
	Total		Total		Total		Total	
Samp. Vol., dscf (corr.)	39.69		19.32		37.32		36.04	
Dry Gas Comp.								
CO ₂ (vol %)		1.8		2.7		2.0		2.2
O ₂ (vol %)		18.5		17.3		18.0		18.3
CO (vol %)		0.0		0.2		0.2		0.3
N ₂ (vol %)		79.7		79.8		79.8		79.2
Moisture, vol%								
M-5		38.94		35.79		31.62		26.53
Sat. at T out		28.61		29.97		29.09		29.87
Mol Wt,								
Dry		29.03		29.13		29.04		29.09
Wet		25.87		25.79		25.83		26.14
Front-half Part., mg		36.97		15.30		26.87		37.98
Back-half Part., mg		1.08		1.41		1.35		2.31
Total DER Part, mg		38.05		16.71		28.22		40.29

**TABLE 5. TOTAL PENNSYLVANIA DER PARTICULATES*
COMPLIANCE TESTS**

Run Number	Number of Pushes	Part. Conc. gr/dscf	Part. Rate, lbs/hr	Part. Rate, lb/ton coke	Allowable, lb/ton coke
7.1	24	0.0167	0.76	0.0144	0.0400
7.2	24	0.0404	2.24	0.0324	0.0400
7.4	24	0.0211	1.26	0.0185	0.0400
7.5	24	0.0146	0.82	0.0128	0.0400
Avg		0.023	1.27	0.020	0.040
Avg w/o No. 7.2		0.017	0.95	0.015	0.040

* Includes total front-half, plus insoluble back-half

**TABLE 6. FRONT-HALF PARTICULATES*
COMPLIANCE TESTS**

Run Number	Number of Pushes	Part. Conc. gr/dscf	Part. Rate, lbs/hr	Part. Rate, lb/ton coke
7.1	24	0.0161	0.73	0.0138
7.2	24	0.0394	2.18	0.0316
7.4	24	0.0204	1.22	0.0178
7.5	24	0.0140	0.78	0.0122
Avg		0.022	1.23	0.019
Avg w/o No. 7.2		0.017	0.91	0.015

* Includes filter and front-half acetone and water washes

**TABLE 7. BACK-HALF PARTICULATES*
COMPLIANCE TESTS**

Run Number	Number of Pushes	Part. Conc. gr/dscf	Part. Rate, lbs/hr	Part. Rate, lb/ton coke
7.1	24	0.00065	0.029	0.00056
7.2	24	0.00103	0.057	0.00083
7.4	24	0.00075	0.045	0.00066
7.5	24	0.00068	0.038	0.00059
Avg		0.00078	0.042	0.00066
Avg w/o No. 7.2		0.00069	0.037	0.00060

* Includes 0.22 micron filter catch of impinger solution

**TABLE 8. TOTAL PENNSYLVANIA DER PARTICULATES*
PRE-COMPLIANCE TESTS**

Run Number	Number of Pushes	Part. Conc. gr/dscf	Part. Rate, lbs/hr	Part. Rate, lb/ton coke	Allowable, lb/ton coke
3.1	24	0.0148	1.00	0.0163	0.0400
3.2	12	0.0133	0.81	0.0140	0.0400
3.3	24	0.0117	0.54	0.0112	0.0400
3.4	24	0.0251	1.48	0.0228	0.0400
Avg		0.016	0.96	0.016	0.040

* Includes total front-half, plus insoluble back-half

**TABLE 9. FRONT-HALF PARTICULATES*
PRE-COMPLIANCE TESTS**

Run Number	Number of Pushes	Part. Conc. gr/dscf	Part. Rate, lbs/hr	Part. Rate, lb/ton coke
3.1	24	0.0144	0.97	0.0158
3.2	12	0.0122	0.74	0.0128
3.3	24	0.0111	0.52	0.0106
3.4	24	0.0236	1.39	0.0215
Avg		0.015	0.90	0.015

* Includes filter and front-half acetone and water washes

**TABLE 10. BACK-HALF PARTICULATES*
PRE-COMPLIANCE TESTS**

Run Number	Number of Pushes	Part. Conc. gr/dscf	Part. Rate, lbs/hr	Part. Rate, lb/ton coke
3.1	24	0.00042	0.028	0.00046
3.2	12	0.00113	0.068	0.00118
3.3	24	0.00056	0.026	0.00053
3.4	24	0.00144	0.085	0.00131
Avg		0.00089	0.052	0.00087

* Includes 0.22 micron filter catch of impinger solution

TABLE 11. SUMMARY OF VISIBLE EMISSION OBSERVATIONS

Test No.	12-5-84 7.1		12-6-84 7.2		12-13-84 7.4		12-14-84 7.5		10-23-84 3.3	
Point No.	Opac >20%	Sec >20%	Opac >20%	Sec >20%	Opac >20%	Sec >20%	Opac >20%	Sec >20%	Opac >20%	Sec >20%
1.6 P	65%	10s								
T										
1.5 P	20	1	70%	3s						
T										
1.4 P			65	5						
T										
1.3 P	65	4								
T					25%	1s				
1.2 P			55	8						
T										
1.1 P					25	1				
T										
2.6 P	20	0.9					65%	1s		
T										
2.5 P			30	1						
T										
2.4 P			80	10						
T										
2.3 P	25	2								
T										
2.2 P			90	9						
T										
2.1 P			65	8						
T										
3.6 P			40	3						
T										
3.5 P			30	2						
T										
3.4 P			80	10			60	3		
T										
3.3 P			85	7						
T										
3.2 P	30	1								
T										
3.1 P			100	21	25	1				
T										
4.6 P			30	2						
T										
4.5 P			35	2	45	5				
T										
4.4 P			95	16						
T										
4.3 P			100	27						
T										
4.2 P			100	8						
T										
4.1 P			30	1						
T										

No./test
Sec/test

6

18.9

18

143

4

17

8

2

4

0

0

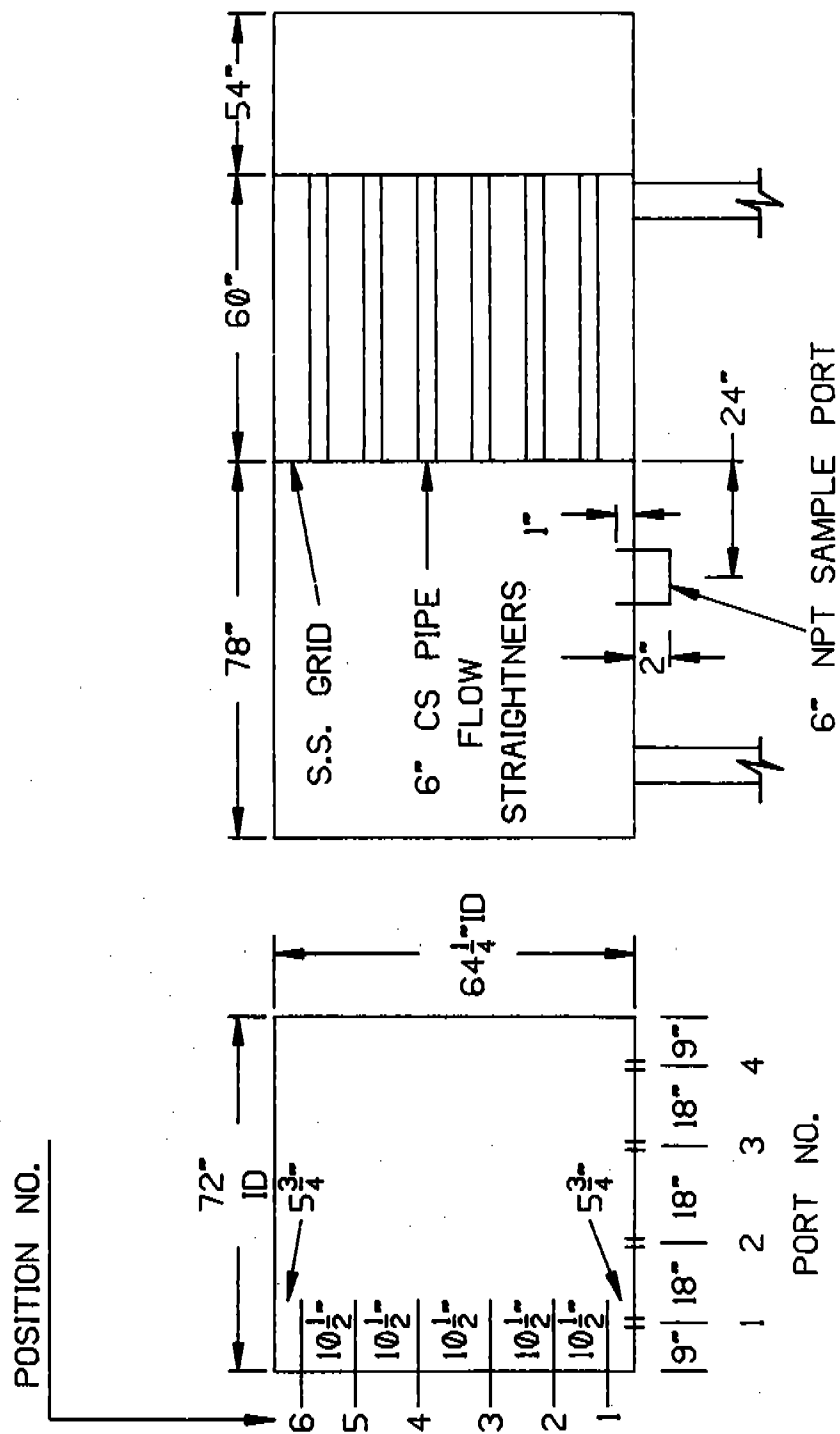


Figure 3. Test Car Duct Sampling Arrangement.

File No. 50.50

2/12/85

**Compliance Tests of the
Envirotech Hooded Quench Car No. 104
Operated on the
Number 20 Coke Battery
Located at the
United States Steel Clairton Works**

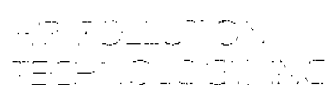
VOLUME II - Appendices

Clairton, PA 15025

Project No. 50.50

February 12, 1985

**Prepared by:
Dr. R.G. Patterson**



APPENDIX A
SCRUBBER OPERATING DATA

BAT. # : 20

OVEN NUMBER	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16
TIME AT START OF PUSH	C-26 10:28	A-28 10:45	B-28 11:06	A-1 11:35	B-1 12:16	C-1 12:29	A-3 12:59	B-3 13:12	C-3 13:23	A-5 14:12	E-5 14:55	C-5 2:09	A-7 2:22	B-7 2:38	C-7 2:51	A-1 2:55
OVEN SCRUBBED (Y or N)	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y
COKING TIME (HRS.)																
LR 505 HOT WATER TANK LEVEL BEFORE PUSH (0-100%)	72%	"	"	"	"	"	"	"	"	"	"	"	"	"	"	"
TR 509 HOT WATER TANK TEMP BEFORE PUSH (0-600°F)	429°	"	"	"	"	"	"	"	"	"	"	"	"	"	"	"
SEPARATOR INLET PRESSURE (IN. W.C.)	11			10.5			10.5			10.5			11.5			
FR 521 FLOW TO JETS (0-600 GPM)	355	"	"	"	"	350				"	"	"	"	"	"	"
PR 522 PRESS. TO JETS (0-500 PSIG)	225	"	"	"	"	"	"	292	"	"	"	"	225	"	"	"
TR 524 TEMP. TO JETS (0-600°F)	TRANS MITTER							WORKING					PROPERLY			
TR 531 COKE GAS TEMP. (0-700°F)	140°	133°	140°	154°	141°	141°	147°	117°	132°	141°	140°	147°	141°	117°	117°	140°
FR 521 FLOW TO JETS																
PR 522 PRESS. TO JETS																
TR 524 TEMP. TO JETS																
TR 531 COKE GAS TEMP.																
FR 521 FLOW TO JETS	115	"	"	"	"	"	"	"	"	"	"	"	"	"	"	"
PR 522 PRESS. TO JETS	281	"	"	"	"	"	"	285	"	"	"	"	287	"	"	"
TR 524 TEMP. TO JETS	TRANS MITTER							WORKING					PROPERLY			
TR 531 COKE GAS TEMP.	133°	126°	133°	140°	176°	132°	133°	76°	119°	06°	116°	133°	133°	133°	172°	176°
ANNUAL MAINT. FULL		2.9		1.95												
ANNUAL MAINT. TRAVEL	1			105						1						
COKE GAS TEMP. AT TWICE	189°	161°	161°	145°	161°	168°	141°	168°	141°	154°	168°	145°	168°	175°	113°	161°

DATE: 12-5-87

CAR # : 4

BAT. # : 20

TEST DESCRIPTION: CAR #4 - TEST 7.1 - OFFICIAL E.P.A. TEST

	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16
OVEN NUMBER	B-9	C-9	A-11	B-11	C-11	A-13	B-13	C-13								
TIME AT START OF PUSH	3:10	3:21	3:43	3:52	4:09	4:21	4:34	4:47								
OVEN SCRUBBED (Y or N)	Y	Y	Y	Y	Y	Y	Y	Y								
COKING TIME (HRS.)																
LR 505 HOT WATER TANK LEVEL BEFORE PUSH (0-100%)	72%	"	"	"	"	"	"	"								
TR 509 HOT WATER TANK TEMP BEFORE PUSH (0-600°F)	429°	"	"	"	"	"	"	"								
SEPARATOR INLET PRESSURE (IN. W.C.)	10.5			10.5				10.5								
FR 521 FLOW TO JETS (0-600 GPM)	350	"	"	"	"	"	"	"								
PR 522 PRESS. TO JETS (0-500 PSIG)	295	"	"	"	"	"	"	"								
TR 524 TEMP. TO JETS (0-600°F)	TRANS MITTER	154°	147°	140°	154°	154°	154°	147°	147°	147°						
TR 531 COKE GAS TEMP. (0-700°F)	147°	154°	147°	140°	154°	154°	154°	147°	147°	147°						
FR 521 FLOW TO JETS																
PR 522 PRESS. TO JETS																
TR 524 TEMP. TO JETS																
TR 531 COKE GAS TEMP.																
FR 521 FLOW TO JETS	115	"	"	"	"	"	"	"								
PR 522 PRESS. TO JETS	287	"	"	"	"	"	"	"								
TR 524 TEMP. TO JETS	TRANS MITTER	133°	133°	133°	133°	133°	133°	133°	133°	133°						
TR 531 COKE GAS TEMP.	133°	133°	133°	133°	133°	133°	133°	133°	133°	133°						
ANNUAL MAINT. FULL	3			7.95				7.95								
ANNUAL MAINT. TRAVEL	1			1				1								
COKE GAS TEMP. AT TWR.	168°	175°	168°	161°	175°	173°	163°	168°	168°	168°						

DATE: 12-6-84

CAR #:

BAS #: 20

TEST DESCRIPTION: CAC #4 - TEST 7.2 - OFFICIAL EPA TEST

	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16
OVEN NUMBER	B-19	C-19	A-21	B-21	C-21	A-23	B-23	C-23								
TIME AT START OF PUSH	1 02	1 15	1 29	1 42	1 54	2 06	2 18	2 31								
OVEN SCRUBBED (Y OR N)	Y	Y	Y	Y	Y	Y	Y	Y								
COKING TIME (HRS)																
I.R. 505 HOT WATER TANK LEVEL BEFORE PUSH (0-100%)	74%	"	"	"	"	"	"	"								
TR 509 HOT WATER TANK TEMP BEFORE PUSH (0-600°F)	429°	"	"	"	"	"	"	"								
SEPARATOR INLET PRESSURE (IN. W.C.)	10.5			10.5				10.5								
FR 521 FLOW TO JETS (0-600 GPM)	350	"	"	"	"	"	"	"								
PR 522 PRESS. TO JETS (0-500 PSIG)	295	"	290	295	"	"	"	"								
TR 524 TEMP. TO JETS (0-600°F)																
TR 531 COKE GAS TEMP. (0-700°F)	147°	147°	133°	140°	154°	147°	140°	147°								
FR 521 FLOW TO JETS																
PR 522 PRESS. TO JETS																
TR 524 TEMP. TO JETS																
TR 531 COKE GAS TEMP.																
FR 521 FLOW TO JETS	115	"	"	"	"	"	"	"								
PR 522 PRESS. TO JETS	287	285	282	285	287	"	"	"								
TR 524 TEMP. TO JETS																
TR 531 COKE GAS TEMP.	126°	133°	119°	140°	140°	133°	133°	126°								
ANALOGAE MARCH FULL	305			305				305								
ANALOGAE MARCH TRAVEL	95			95				95								
OVER FAS. TEMP. TO TRAVEL	118°	157°	161°	175°	210°	210°	210°	118°								

TR 524

TR 531

TR 524

DATE: 12-6-84

CAR #:

BAT. #:

TEST DESCRIPTION: CAC#4 - TEST 7.2 - OFFICIAL E.P.A. TEST

	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16
OVEN NUMBER	A-9	B-9	C-9	A-11	B-11	C-11	A-13	B-13	C-13	A-15	B-15	C-15	A-17	B-17	C-17	A-19
TIME AT START OF PUSH	9:41	9:53	10:06	10:18	10:30	10:42	10:55	11:07	11:19	11:31	11:43	11:55	12:07	12:19	12:31	12:43
OVEN SCRUBBED (Y or N)	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y
COKING TIME (HRS.)																
IR 505 HOT WATER TANK LEVEL BEFORE PUSH (0-100%)	74%	74%	"	"	"	"	"	"	"	"	"	"	"	"	"	"
TR 509 HOT WATER TANK TEMP BEFORE PUSH (0-600°F)	429°	"	"	"	"	"	"	"	"	"	"	"	"	"	"	"
SEPARATOR INLET PRESSURE (IN. W.C.)		10.5			10.5			10.5			10.5			10.5		
FR 521 FLOW TO JETS (0-600 GPM)	380	"	"	"	"	"	"	"	"	"	"	"	"	"	"	"
PR 522 PRESS. TO JETS (0-500 PSIG)	212	295	"	297	"	295	"	"	"	"	"	"	"	"	"	"
TR 524 TEMP. TO JETS (0-600°F)																
TR 531 COKE GAS TEMP. (0-700°F)	147°	154°	147°	147°	147°	147°	147°	154°	147°	147°	140°	140°	140°	147°	140°	140°
FR 521 FLOW TO JETS																
PR 522 PRESS. TO JETS																
TR 524 TEMP. TO JETS																
TR 531 COKE GAS TEMP																
FR 521 FLOW TO JETS	115	"	"	"	"	"	"	"	"	"	"	"	"	"	"	"
PR 522 PRESS. TO JETS	285	287	"	290	"	"	"	287	"	"	"	"	"	"	"	"
TR 524 TEMP. TO JETS																
TR 531 COKE GAS TEMP	133°	140°	140°	133°	133°	133°	133°	126°	133°	126°	126°	126°	126°	126°	133°	126°
ANNUAL MAINT. FULL		3			3			3			3			3		
ANNUAL MAINT. TRAVEL			1		1			.95			.95			.95		
COKE GAS TEMP. FULL	162°	182°	210°	168°	187°	176°	175°	182°	175°	161°	168°	187°	161°	161°	196°	161°

INLET

INTERMEDIATE

OUTLET

DATE: 12-13-84

Description: CAR#4 - TEST 114 - OFFICIAL EPA TEST

CAR # : 4

BAT # : 20

		1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16
OVEN NUMBER		B-1	C-1	A-3	B-3	C-3	A-5	B-5	C-5	A-7	B-7	C-7	A-9	B-9	C-9	A-11	B-11
TIME AT START OF PUSH		9:30	9:42	9:57	10:09	10:21	10:35	10:47	10:59	11:11	11:21	11:36	11:49	12:02	12:17	12:29	12:41
OVEN SCRUBBED (Y OR N)		Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y
COKING TIME (HRS)																	
LR 505 HOT WATER TANK LEVEL BEFORE PUSH (0-100%)		74%	"	"	"	"	"	"	"	"	"	"	"	"	"	"	"
TR 509 HOT WATER TANK TEMP BEFORE PUSH (0-600°F)		414°	"	"	"	"	"	"	"	"	"	"	"	"	"	"	"
SEPARATOR INLET PRESSURE (IN. W.C.)		"	"	"	"	"	"	"	"	"	"	"	"	"	"	"	"
FR 521 FLOW TO JETS (0-600 GPM)		265	"	"	"	360	"	"	265	"	"	"	"	370	365	"	"
PR 522 PRESS. TO JETS (0-500 PSIG)		295	"	"	"	"	"	"	"	"	"	"	"	"	"	"	"
TR 524 TEMP. TO JETS (0-600°F)		203°	210°	139°	189°	199°	199°	203°	196°	189°	189°	210°	196°	203°	203°	196°	203°
FR 521 FLOW TO JETS																	
PR 522 PRESS. TO JETS																	
TR 524 TEMP. TO JETS																	
TR 531 COKE GAS TEMP.																	
FR 521 FLOW TO JETS		115	"	"	"	"	"	"	"	"	"	"	"	"	"	"	"
PR 522 PRESS. TO JETS		287	"	"	"	"	"	"	"	287	"	"	"	"	"	"	285
TR 524 TEMP. TO JETS																	
TR 531 COKE GAS TEMP.																	
FR 521 FLOW TO JETS		175°	187°	175°	175°	163°	175°	163°	175°	168°	168°	189°	168°	175°	175°	168°	175°
PR 522 PRESS. TO JETS		2.1	2.1			2.1			3.05			3.05			3.05		
TR 524 TEMP. TO JETS									1.5			1.45			1.45		
TR 531 COKE GAS TEMP.																	
UNDERK MAND FULL																	
UNDERK MAND. TRAVEL																	
PRE 525 TEMP. TO JETS		210°	210°	196°	196°	196°	196°	196°	203°	196°	210°	210°	210°	210°	210°	203°	203°

TOP

INTERMEDIATE

BOTTOM

DATE: 12-13-84

CAR #:

4

BAT. #:

20

TEST DESCRIPTION: CAR#4 - TEST 7.4 - OFFICIAL E.P.A. TEST

OVEN NUMBER	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16
TIME AT START OF PUSH	C-11	A-13	B-13	C-13	A-15	B-15	C-15	A-17								
	12 ⁵³	109	126	133	145	158	210	223								
OVEN SCRUBBED (Y or N)	Y	Y	Y	Y	Y	Y	Y	Y								
COKING TIME (HRS)																
LR 505 HOT WATER TANK LEVEL BEFORE PUSH (0-100%)	74 ¹⁰	"	"	"	"	"	"	"								
TR 509 HOT WATER TANK TEMP BEFORE PUSH (0-600°F)	414 ⁰	"	"	"	"	"	"	"								
SEPARATOR INLET PRESSURE (IN. W.G.)	11			11												
FR 521 FLOW TO JETS (0-600 GPM)	365	"	"	"	"	"	"	"								
PR 522 PRESS. TO JETS (0-500 PSIG)	295	"	"	"	"	"	"	"								
TR 524 TEMP. TO JETS (0-600°F)	203	203	203	203	196	196	196	203	INOPERABLE							
TR 531 COKE GAS TEMP. (0-700°F)	203	203	203	203	196	196	196	203								
FR 521 FLOW TO JETS									INOPERABLE							
PR 522 PRESS. TO JETS																
TR 524 TEMP. TO JETS																
TR 531 COKE GAS TEMP.																
FR 521 FLOW TO JETS	115	"	"	"	"	"	"	"								
PR 522 PRESS. TO JETS	234	"	"	"	"	"	"	"								
TR 524 TEMP. TO JETS	175	175	175	175	175	175	175	175	INOPERABLE							
TR 531 COKE GAS TEMP.	175	175	175	175	175	175	175	175								
MINIMUM MAINT. FUEL	2.05			3.05												
MINIMUM MAINT. TRAVEL	1.5			1.5												
MINIMUM TRAVEL TIME	179	196	196	217	207	207	207	196								

PUSHING SCHEDULE FOR BATTERIES 19/20

SEQ #	PUSH	CHARGE	STATION	EARLIEST	DESIRED	LATES
1	A26/19	A24/19		7:53	8:00	8:14
2	A26/20	A24/20		7:59	8:06	8:20
3	B26/19	B24/19		8:05	8:12	8:26
4	B26/20	B24/20		8:11	8:18	8:32
5	C26/19	C24/19		8:18	8:25	8:39
6		C24/20		8:24	8:31	8:45
7		A26/19		8:30	8:37	8:51
8		A26/20		8:37	8:44	8:58
9		B26/19		8:43	8:50	9:04
10		B26/20		8:49	8:56	9:10
11		C26/19		8:56	9:03	9:17
12		C26/20		9:02	9:09	9:23
13		A28/19		9:08	9:15	9:29
14		A28/20		9:15	9:22	9:36
15		B28/19		9:21	9:28	9:42
16		B28/20		9:27	9:34	9:48
17		C28/19		9:34	9:41	9:55
18		C28/20		9:40	9:47	10:01
19		A1/19		9:46	9:53	10:07
20		A1/20		9:52	9:59	10:13
21		B1/19		9:59	10:06	10:20
22		B1/20		10:05	10:12	10:26
23		C1/19		10:11	10:18	10:32
24		C1/20		10:18	10:25	10:39
25		A3/19		10:24	10:31	10:45
26		A3/20		10:30	10:37	10:51
27		B3/19		10:37	10:44	10:58
28		B3/20		10:43	10:50	11:04
29		C3/19		10:49	10:56	11:10
30		C3/20		10:56	11:03	11:17
31		A5/19		11:02	11:09	11:23
32		A5/20		11:08	11:15	11:29
33		B5/19		11:15	11:22	11:36
34		B5/20		11:21	11:28	11:42
35		C5/19		11:27	11:34	11:48
36		C5/20		11:34	11:41	11:55
37		A7/19		11:40	11:47	12:01
38		A7/20		11:46	11:53	12:07
39		B7/19		11:53	11:59	12:13
40		B7/20		11:59	12:06	12:20
41		C7/19		12:05	12:12	12:26
42		C7/20		12:11	12:18	12:32
43		A9/19		12:18	12:25	12:39
44		A9/20		12:24	12:31	12:45
45		B9/19		12:30	12:37	12:51
46		B9/20		12:37	12:44	12:58
47		C9/19		12:43	12:50	13:04
48		C9/20		12:49	12:56	13:10
49		A11/19		12:56	13:03	13:17
50		A11/20		13:02	13:09	13:23
51		B11/19		13:08	13:15	13:29
52		B11/20		13:15	13:22	13:36
53		C11/19		13:21	13:28	13:42
54		C11/20		13:27	13:34	13:48
55		A13/19		13:34	13:41	13:55
56		A13/20		13:40	13:47	14:01
57		B13/19		13:46	13:53	14:07
58		B13/20		13:53	13:59	14:13
59		C13/19		13:59	14:06	14:20
60		C13/20		14:05	14:12	14:26
61		A15/19		14:11	14:18	14:32
62		A15/20		14:18	14:25	14:39
63		B15/19		14:24	14:31	14:45
64		B15/20		14:30	14:37	14:51
65		C15/19		14:37	14:44	14:58
66		C15/20		14:43	14:50	15:04
67		A17/19		14:49	14:56	15:10
68		A17/20		14:56	15:03	15:17
69		B17/19		15:02	15:09	15:23
70	B19/20	B17/20		15:08	15:15	15:29
71	C19/19	C17/19		15:15	15:22	15:36
72	C19/20	C17/20		15:21	15:28	15:42
73	A21/19	A19/19		15:27	15:34	15:48
74	A21/20	A19/20		15:34	15:41	15:55
75	B21/19	B19/19		15:40	15:47	16:01
76	B21/20	B19/20		15:46	15:53	16:07

THR DEC 13 1984

BX 4 TURN

A-5-19 Batt
A-28-20 Batt > EMPTY Patches

DATE: 12-14-80
CAR #: 4
BAT #: 20

TEST DESCRIPTION: CAR #4 - TEST 7.5- OFFICIAL EPA TEST

	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16
OVEN NUMBER	A-27	B-27	C-27	A-29	B-29	H-2	B-2	C-2	A-4							
TIME AT START OF PUSH	12:23	12:36	12:48	1:01	1:14	1:40	1:58	2:44	2:24							
OVEN SCRUBBED (Y or N)	Y	Y	Y	Y	Y	Y	Y	Y	Y							
COKING TIME (HRS.)																
LR 505 HOT WATER TANK LEVEL BEFORE PUSH (0-100%)	72%	"	"	"	"	"	64%	72%	"							
TR 509 HOT WATER TANK TEMP BEFORE PUSH (0-600°F)	414°	"	"	"	"	"	"	"	"							
SEPARATOR INLET PRESSURE (IN. W.C.)	11			11				11								
FR 521 FLOW TO JETS (0-600 GPM)	360	"	"	"	"	355	315	360	"							
PR 522 PRESS. TO JETS (0-500 PSIG)	795	"	"	"	"	"	215	295	"							
TR 524 TEMP. TO JETS (0-600°F)																
TR 531 COKE GAS TEMP. (0-700°F)	203°	196°	196°	203°	203°	196°	154°	196°	182°							
FR 521 FLOW TO JETS																
PR 522 PRESS. TO JETS																
TR 524 TEMP. TO JETS																
TR 531 COKE GAS TEMP.																
FR 521 FLOW TO JETS	150	"	"	"	"	"	115	120	"							
PR 522 PRESS. TO JETS	231	"	"	"	"	"	110	281	"							
TR 524 TEMP. TO JETS																
TR 531 COKE GAS TEMP.																
APPROX. FLOW. TO CC	3.05			3.05				3.05								
APPROX. FLOW. TO JET	1.4			1.35												
APPROX. FLOW. TO JET	3.17°	2.77°	2.10°	2.14°	2.10°	1.1°	1.89°	2.24°								

TRANSFERABLE

TRANSFERABLE

DATE: 4/84
CAR #: 4
BAT. #: 20

TEST DESCRIPTION: C.H.K. - 7

ACTIVATION: APR 1 1984

TEST 3-1
4 5 6 7 8 9 10 11 12 13 14 15 16

OVEN NUMBER	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16
C-21	A-23	B-23	C-23	A-15	B-25	C-25	A-17	B-27	C-27	A-29	B-29	C-29	A-2	B-2	C-2	
TIME AT START OF PUSH	11:26	11:50	12:03	12:17	12:30	12:43	12:57	1:10	1:23	1:36	1:49	2:02	2:15	2:28	2:41	2:54
OVEN SCRUBBED (Y or N)	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y
COKING TIME (HRS.)																
LR 505 HOT WATER TANK LEVEL BEFORE PUSH (0-100%)	73%	78%	73%	73%	73%	73%	73%	78%	78%	78%	78%	78%	"	"	"	"
TR 505 HOT WATER TANK TEMP BEFORE PUSH (0-600°F)	420°	420°	426°	426°	426°	426°	432°	432°	432°	432°	432°	432°	"	"	"	"
SEPARATOR INLET PRESSURE (IN. W.C.)		12					11	10	10.5							
FR 521 FLOW TO JETS (0-600 GPM)	400	400	400	408	403	403	403	400	400	400	400	400	"	"	"	"
PR 522 PRESS. TO JETS (0-500 PSIG)	290	290	295	270	295	295	305	300	300	300	300	300	"	"	"	"
TR 524 TEMP. TO JETS (0-600°F)	420°	420°	420°	420°	420°	420°	420°	420°	426°	420	420	420	"	"	"	414
TR 531 COKE GAS TEMP. (0-700°F)	1549°	1549°	1470°	1460°	1460°	1460°	1333°	140	140	140	140	154	140	140	140	"
FR 521 FLOW TO JETS																
PR 522 PRESS. TO JETS																
TR 524 TEMP. TO JETS																
TR 531 COKE GAS TEMP.																
FR 521 FLOW TO JETS	110	110	110	110	110	110	110	110	110	110	110	110	110	110	110	110
PR 522 PRESS. TO JETS	275	280	285	230	285	285	290	280	280	280	280	280	280	280	280	280
TR 524 TEMP. TO JETS	420°	420°	420°	420°	420°	420°	420°	420	420	420	420	420	420	420	420	420
TR 531 COKE GAS TEMP.	1471°	1471°	1471°	1471°	1471°	1471°	1471°	1471°	1471°	1471°	1471°	1471°	1471°	1471°	1471°	1471°
APPROX. MIN. FULL	4.0						2.2	2.6	2.6	2.5			2.5			
MINIMUM TRAVEL	1.6						1.2		1.2				1.2			
COKE GAS TEMP. AT JWK.	115°	273°	251°	273°	410°	410°	410°	410°	410°	410°	410°	410°	410°	410°	410°	410°

~~57845 54555~~
~~57845 54555~~

DATE: 7-84
CAR #: 4
BAL. #: 20

TEST DESCRIPTION: C/H/C + 4

TURNITION SPRAY RES #1
Test 3-1

OVEN NUMBER	A-4	B-4	C-4	A-6	B-6	C-6	A-8	B-8	A-10
TIME AT START OF PUSH	326	339	352	403	414	426	438	449	516
OVEN SCRUBBED (Y or N)	Y	Y	Y	Y	Y	Y	Y	Y	Y
COKING TIME (HRS.)									
LR 505 HOT WATER TANK LEVEL BEFORE PUSH (0-100%)	78	"	"	"	"	"	"	"	"
TR 509 HOT WATER TANK TEMP BEFORE PUSH (0-600°F)	426	"	"	"	"	"	"	"	"
SEPARATOR INLET PRESSURE (IN. W.C.)	10					15		12	12
FR 521 FLOW TO JETS (0-600 GPM)	400	"	"	"	"	"	"	"	"
PR 522 PRESS. TO JETS (0-500 PSIG)	300	"	"	"	"	"	"	"	"
TR 524 TEMP. TO JETS (0-600°F)	414	"	"	"	"	"	1108	420	"
TR 531 COKE GAS TEMP. (0-700°F)	126	140	147	140	140	133	140	138	140
FR 521 FLOW TO JETS									
PR 522 PRESS. TO JETS									
TR 524 TEMP. TO JETS									
TR 531 COKE GAS TEMP.									
FR 521 FLOW TO JETS	110	"	"	"	"	"	"	"	"
PR 522 PRESS. TO JETS	240	"	"	"	"	"	"	"	"
TR 524 TEMP. TO JETS	414	"	"	"	"	"	408	420	"
TR 531 COKE GAS TEMP.	154	154	168	154	154	154	140	140	154
HUNDERAL PRESS. FULL	CCTT								
HUNDERAL PRESS. TAIL	CCTT								
COKE GAS TEMP. AT TWR.	176	196	224	176	196	217	183	154	161

DATE: 10-21-84
CAR #: 20
BAT. #: 20

TEST DESCRIPTION: CAMEL SUPERHEATON SPRAY 1051-2
Test 3-2

OVEN NUMBER	1 2 3 4 5 6 7 8 9 10 11 12											
	A-24	B-24	C-24	A-26	B-26	C-26	B-28	C-28	A-1	B-1	A-3	B-3
TIME AT START OF PUSH	112	124	130	151	203	215	247	258	311	329	352	404
OVEN SCRUBBED (Y or N)	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y
COKING TIME (HRS.)												
LR 505 HOT WATER TANK LEVEL BEFORE PUSH (0-100%)	118%	"	"	"	"	"	"	"	"	"	"	"
TR 509 HOT WATER TANK TEMP BEFORE PUSH (0-600°F)	432°	"	"	"	"	"	"	"	"	"	"	"
SEPARATOR INLET PRESSURE (IN. W.C.)	12	12			12			12			12	
FR 521 FLOW TO JETS (0-600 GPM)	400	"	"	"	"	"	400		"	360	400	
PR 522 PRESS. TO JETS (0-500 PSIG)	305	"	"	"	"	"	310		"	385	305	
TR 524 TEMP. TO JETS (0-600°F)	420°	"	426°	437°			420°	426°	"	"	420°	
TR 531 COKE GAS TEMP. (0-700°F)	140°	140°	133°	140°		137°	141°	140°	168°	140°	147°	
FR 521 FLOW TO JETS												
PR 522 PRESS. TO JETS												
TR 524 TEMP. TO JETS												
TR 531 COKE GAS TEMP.												
FR 521 FLOW TO JETS	110	"	"	"	"	"	"	"	"	"	"	"
PR 522 PRESS. TO JETS	225	"	"	"	"	"	300	"	"	275	300	225
TR 524 TEMP. TO JETS	420°	"	426°	432°	"	410°	470°	426°	"	"	"	420°
TR 531 COKE GAS TEMP.	141°	140°	140°	140°	147°	140°	141°	147°	141°	149°	147°	149°
FLOWER Neck Temp	2.7	2.85			2.8	2.15		3.0			2.8	
Ambient Neck Temp				1.1	1.4			1.25				
COKE GAS TEMP. AT TOWER	132°	175°	192°	111°	182°	187°	154°	187°	161°	161°	161°	161°

DATE: 1-23-84
CAR #: 7
BAT. #: 20

TEST DESCRIPTION: CARBONIZATION

SPRAY TEST #3

Test 3-3

OVEN NUMBER	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16
A-17	B-17	C-17	A-19	B-19	C-19	A-21	B-21	C-21	A-23	B-23	C-23	A-25	B-25	C-25	A-29	
TIME AT START OF PUSH	12:36	12:50	1:03	1:20	1:33	1:46	2:02	2:16	2:36	2:53	3:06	3:18	3:32	3:46	3:59	4:48
OVEN SCRUBBED (Y or N)	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y
COKING TIME (HRS)																
LR 505 HOT WATER TANK LEVEL BEFORE PUSH (0-100%)	77%	"	"	74%	77%	"	"	"	75%	74%	75%	77%	"	"	"	"
TR 505 HOT WATER TANK TEMP BEFORE PUSH (0-600°F)	432°	"	"	"	"	"	"	"	429°	"	"	"	"	"	"	"
SEPARATOR INLET PRESSURE (IN. W.C.)		12			12			12						12		
FR 521 FLOW TO JETS (0-600 GPM)	408		400	226		296	"	315	375	360	375	"	"	"	"	"
PR 522 PRESS. TO JETS (0-500 PSIG)	305	"	310	275	310	285	"	300	285	285	295	"	"	"	"	"
TR 524 TEMP. TO JETS (0-600°F)	408°	476°	408°	444°	"	425°	444°	420°	476°	"	423°	420°	"	426°	420°	"
TR 531 COKE GAS TEMP. (0-700°F)	147°	140°	140°	126°	140°	119°	111°	122°	126°	133°	146°	154°	147°	147°	161°	168°
FR 521 FLOW TO JETS																
PR 522 PRESS. TO JETS																
TR 524 TEMP. TO JETS																
TR 531 COKE GAS TEMP.																
FR 521 FLOW TO JETS	110	110	110	"	"	"	"	"	"	"	"	"	"	"	"	"
PR 522 PRESS. TO JETS	295	"	300	285	300	275	"	220	215	275	285	"	"	"	"	"
TR 524 TEMP. TO JETS	414°	425°	408°	444°	"	425°	444°	420°	476°	423°	420°	"	426°	420°	"	"
TR 531 COKE GAS TEMP.	140°	140°	140°	133°	140°	119°	111°	122°	126°	133°	147°	147°	147°	147°	177°	147°
ANALYST: MARIO FULL		I	NO													
ANALYST: MARIO TEAVEZ		I														
COKE GAS TEMP. TO TANK	154°	175°	192°	149°	115°	109°	123°	128°	125°	147°	143°	175°	161°	163°	182°	163°

DATE: 12-84

CAR #:

BAT. #: 20

TEST DESCRIPTION: CAR #4

ON SPRAY TEST #3 (CONT.)

TEST 3-3

OVEN NUMBER	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16
TIME AT START OF PUSH	B-29	C-29	A-2	B-2	C-2	A-4	B-4	C-4								
OVEN SCRUBBED (Y OR N)	Y	Y	Y	Y	Y	Y	Y	Y								
COKING TIME (HRS.)																
L.R. 505 HOT WATER TANK LEVEL BEFORE PUSH (0-100%)	77%	"	"	"	"	"	76%	"								
TR 509 HOT WATER TANK TEMP BEFORE PUSH (0-600°F)	129°	"	"	"	"	"	"	"								
SEPARATOR INLET PRESSURE (IN. W.C.)	12			12			12									
FR 521 FLOW TO JETS (0-600 GPM)	375	"	"	"	"	"	"	"								
PR 522 PRESS. TO JETS (0-500 PSIG)	295	"	"	"	"	"	"	"								
TR 524 TEMP. TO JETS (0-600°F)	420°	"	410°	"	402°	330°	410°	"								
TR 531 COKE GAS TEMP. (0-700°F)	161°	154°	163°	154°	154°	154°	147°	154°								
FR 521 FLOW TO JETS																
PR 522 PRESS. TO JETS																
TR 524 TEMP. TO JETS																
TR 531 COKE GAS TEMP.																
FR 521 FLOW TO JETS	110	"	"	"	"	"	"	"								
PR 522 PRESS. TO JETS	18	"	"	"	"	"	"	"								
TR 524 TEMP. TO JETS	160°	"	110°	"	402°	110°	"	"								
TR 531 COKE GAS TEMP.	17°	140°	117°	147°	140°	147°	140°	140°								
ANALOG MAND. FUEL																
ANALOG MAND. TURBID																
COKE GAS TEMP. AT TANK	162°	189°	161°	173°	175°	177°	163°	191°								

DATE: 10-1-84
 CAR #: 4
 BAT. #: 20

TEST DESCRIPTION: CARBON SATURATION SPRAY TEST #4

10-24-84

Test # 3-4

OVEN NUMBER	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16
TIME AT START OF PUSH	C-25 9:57	A-27 10:11	B-27 10:23	C-27 10:35	A-29 10:49	B-29 11:02	C-29 11:28	A-2 11:33	B-2 11:57	C-2 12:09	A-4 12:22	B-4 12:34	C-4 12:47	A-6 12:59	B-6 1:11	C-6 1:24
OVEN SCRUBBED (Y or N)	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y	Y
COKING TIME (HRS.)																
LR 505 HOT WATER TANK LEVEL BEFORE PUSH (0-100%)	16%	"	"	"	"	"	"	"	"	"	"	"	"	"	"	"
TR 509 HOT WATER TANK TEMP BEFORE PUSH (0-600°F)	426°	429°	"	"	"	"	426	429°	"	"	"	"	"	"	"	"
SEPARATOR INLET PRESSURE (IN. W.C.)	"			11.5			10.5			11.5			"			
FR 521 FLOW TO JETS (0-600 GPM)	395	"	"	"	"	"	"	"	"	"	"	"	"	"	"	"
PR 522 PRESS. TO JETS (0-500 PSIG)	287	290	295	297	295	"	300	295	"	"	297	"	300	297	"	292
TR 524 TEMP. TO JETS (0-600°F)	408	414°	417°	420°	423°	426°	426	429°	420°	426°	429°	426°	429°	426°	429°	426°
TR 531 COKE GAS TEMP. (0-700°F)	417°	417°	417°	461°	461°	461°	"	462°	475°	461°	468°	482°	475°	482°	461°	454°
FR 521 FLOW TO JETS																
PR 522 PRESS. TO JETS																
TR 524 TEMP. TO JETS																
TR 531 COKE GAS TEMP.																
FR 521 FLOW TO JETS	110	"	"	"	"	"	110	"	"	"	"	"	"	"	"	"
PR 522 PRESS. TO JETS	280	"	285	287	285	"	295	285	"	"	"	287	280	292	287	285
TR 524 TEMP. TO JETS	408°	414°	417°	420°	423°	426°	426	429°	420°	426°	429°	426°	429°	426°	429°	426°
TR 531 COKE GAS TEMP.	417°	417°	417°	461°	461°	461°	462°	462°	475°	461°	468°	482°	475°	482°	461°	454°
APPROX. H2O. FLOW	2.6			2.7			2.6			2.7			2.65			
APPROX. H2O. TANK L.		135			1.7			1.4			1.2			1.3		
COKE GAS TEMP. TANK	196°	192°	182°	110°	167°	137°	210	162°	163°	115°	161°	169°	192°	161°	161°	161°

APPENDIX B
SAMPLE TRAIN DATA SHEETS

Plant USS-CALIBRATION, PA
 Date 12-5-84
 Sample Location HQRR-TEST CAR
 Sample Type M-5
 Run Number 7.1
 Operator IREMMD/SMITH
 Ambient Temperature ~ 29°F
 Barometric Pressure 37.42 @ 4:00P
 Static Pressure, (H₂O) _____
 Filter Number(s) BA1026-045

Impinger Volumes
 Initial Final
 { 100 356.0 } Net Gain 256.0
 { 100 140.0 } 40.0
 { m/f 1.0 } 1.0
 { 100 101.0 } 1.0
 { 100 100.0 } 0
 { m/f 0.0 } 0
 Silica Gel
6823 6914
7360 7435

Probe Length and Type S' TEE LINED
 Nozzle Size & I.D. 287.283 (302)
 Pilot Coefficient & I.D. .84
 Assumed Moisture _____
 Molecular Weight, Dry, (M_d) _____
 Meter Box Number APT 12 LG
 Meter Coefficient _____
 α Factor _____

$K = \frac{K(M_d)^4}{(T_s)^4} \times ()^4 =$
 $\Delta H = K(M_d)^4 \left(\frac{T_m}{T_s} \right) (P)$

SASS Condensate N/A
 Total Volume _____

Leak Check: Initial at 16 Hg, .004 CFM
 Final at 15 Hg, .004 CFM
 Pilot Leak Check: OK

P.H. - 3.5

PAGE- 4,17 → 15.00

Temperature of	PUSH	STACK	Probe	Impinger	FILTER	Oven	Gas Meter		Pump	Avg.	Δ
							In	Out			
Rotometer	Desired	Actual	Velocity Head (AP) in. H ₂ O	Gas Meter Reading (V _m), ft ³	MIN:SEC	Sampling Time, min	Traverse Point Number				
				Init. 288.474							
			.80	287.21	:44						
			.25	289.737	:55						
			.50	290.31	:45						
			.20	290.607	:43						
			.45	291.15	:44						
			.20	291.508	:49						
			.80	292.30	:45						
			.20	292.638	:38						
Avg.											

Traverse Point Number	MIN:SEC Sampling Time, min	Gas Meter Reading (V _m), ft ³ Init. 292.638	Velocity Head (ΔP _s), in. H ₂ O	ROTCMETER		Temperature of					Pump Vacuum In. Hg	Avg. ΔP	Δ H
				Desired	Actual	PUSH STACK TRAVEL	Probe	Impingng	FILTER TEMP	Oven			
1-2	:45	292.638 292.638	1.0		21.1	156	265	40 40		267	44 43	4	.58
	:47	393.45	.25		7.8	156	269	39 39		265	45 43	1	.13
1-1	:47	394.92	1.7	28.1	27.0	159	265	40 40		266	45 44	6	.81
	:46	395.530	.40		12.8	162	263	40 40		267	45 43	2	.21
2-6	:44	397.657	1.3		24.0	155	268	40 40		265	45 44	5	.70
	:32	398.035	.35		11.9	169	270	39 40		268	46 44	1	NA
2-5	:46	298.92	1.2		23.2	155	268	40 40		263	45 45	5	.65
	:46	299.468	.30		10.9	158	270	40 40		266	46 44	1	.19
2-4	:47	300.43	1.4		25.2	152	268	40 40		260	46 45	5.5	.74
	:51	301.063	.40		12.8	160	270	39 39		262	46 44	1	.26
2-3	:47	302.00	1.3		24.2	154	267	40 40		262	46 45	5	.70
	:37	302.425	.35		11.9	159	268	39 39		269	46 44	1	.20
2-2	:46	303.41	1.4		25.2	156	266	40 40		270	46 45	6	.75
	:48	304.65	.50		14.5	157	267	40 40		270	46 45	2	.30
2-1	:46	305.04		30.9 27.0	27.0	156	266	40 40		270	46 46	6	.80
	:53	305.717		30.9 12.8	12.8	158	267	40 40		268	47 45	2	.28
AUG.													

Run No. 7.1

Date 12-5-84

Sampling Location HCRC - TEST SDR

Comments: 1) Could not pull my desired rate. 4) ORSAT Back on
2) ORSAT off for repair.
3) Initial Gas meter reading for this point was 397.017 (397.65 was end of push reading)

Traverse Point Number	MIN:SEC Sampling Time, min	Gas Meter Reading (V _m), ft ³ Init. 305.717	Velocity Head (ΔP _h), in. H ₂ O	ROTOMETER		Temperature of					Gas Meter		Pump Vacuum in. Hg	Avg. ΔP	Δ H
				Desired	Actual	PUSH STACK TRANSEL	Probe	Impedance	FILTER TEMP	Oven	In	Out			
3-6	3:46	306.72	1.6		27.0	154	270	40		266	47	46	6		83
	3:38	307.159	.35		11.9	157	271	40		266	47	45	1		21
3-5	3:45	308.17	1.6		27.0	154	268	41		262	47	46	6		85
	3:45	308.720	.30		16.9	155	271	40		268	48	46	1		23
3-4	3:46	309.54	.95		20.5	154	268	40		270	48	46	NA		54
	3:59	310.051	.25		9.8	157	271	40		270	48	46	1		13
3-3	3:46	310.84	.80		18.7	156	267	40		263	48	47	3		46
	3:41	311.123	.20		.11	158	271	40		267	48	47	1		11
3-2	3:44	311.93	.95		20.5	155	267	40		267	48	47	4		55
	3:45	312.331	.25		9.8	157	270	40		270	48	47	1		14
3-1	3:46	313.19	1.1		22.2	157	266	40		270	48	47	NA		62
	3:54	313.674	.25		9.8	159	269	40		269	48	47	1		14
4-6	3:43	314.37	.80		18.7	154	265	40		266	48	47	3		45
	3:45	314.776	.25		9.8	156	270	40		253	49	47	1		13
4-5	3:45	315.42	.55		15.3	157	268	41		270	49	48	2		53
	3:45	315.670	.15		0.80H	155	271	41		223	49	47	NA		08
AUG.															

Run No.

7.1

Date 12-5-84

Sampling Location HCLC - TEST CAR

1) Static taken part #3 push = .10
travel = .03

Comments:

[illegible]

Run No. 7.1

Date 12-5-84

Sampling Location HCRG - TEST CAR

Comments: H_2O in Pitot Line - no gas meter reading taken at end of push
no time for push taken

DATE - 12-5-84

RUN # - 7.1

PLANT - USS - CLAIRTON

RAW SE POINT	OVEN NUMBER	ΔP EXPECTED	ΔP ACTUAL	ROTOR METER DESIRED	POINT SAMPLE TIME	COMMENT
1.6	C-26	.80	.80	18.7	1:41	
1.5	A-28	.50	.50	14.5	1:28	
1.4	B-28	.45	.45	13.7	1:33	
1.3	A-1	.80	.80	18.7	1:23	
1.2	B-1	1.0	1.0	21.1	1:32	
1.1	C-1	1.7	1.7	28.6	1:33	
2.6	A-3	1.3	1.3	24.2	1:18	
2.5	B-3	1.2	1.2	23.2	1:32	
2.4	C-3	1.4	1.4	25.2	1:38	
2.3	A-5	1.3	1.3	24.2	1:24	
2.2	B-5	1.4	1.4	25.2	1:34	
2.1	C-5	1.7	1.7	27.9	1:39	
3.6	A-7	1.6	1.6	27.0	1:24	
3.5	B-7	1.6	1.6	27.0	1:30	
3.4	C-7	.95	.95	20.5	1:45	
3.3	A-9	.80	.80	18.7	1:27	
3.2	B-9	.95	.95	20.5	1:31	
3.1	C-9	1.1	1.1	22.2	1:40	
4.6	A-11	.80	.80	18.7	1:28	
4.5	B-11	.55	.55	15.3	1:31	
4.4	C-11	.80	.80	18.7	1:40	
4.3	A-13	1.5	1.5	26.2	1:24	
4.2	B-13	1.5	1.5	26.2	1:32	
4.1	C-13	1.2	1.2	23.2	1:39	
Avg.					TOTAL TIME	

ROTOR METER	POINT	ROTOR METER
18.7	1:41	18.7
14.5	1:28	14.5
13.7	1:33	13.7
18.7	1:23	18.7
21.1	1:32	21.1
28.6	1:33	28.6
24.2	1:18	24.2
23.2	1:32	23.2
25.2	1:38	25.2
24.2	1:24	24.2
25.2	1:34	25.2
27.9	1:39	27.9
27.0	1:24	27.0
27.0	1:30	27.0
20.5	1:45	20.5
18.7	1:27	18.7
20.5	1:31	20.5
22.2	1:40	22.2
18.7	1:28	18.7
15.3	1:31	15.3
18.7	1:40	18.7
26.2	1:24	26.2
26.2	1:32	26.2
23.2	1:39	23.2

DRY MOLECULAR WEIGHT DETERMINATION

PLANT USS-CLAUDET
 DATE 12-5-84 TEST No 7.1
 SAMPLING TIME (24 hr CLOCK) _____
 SAMPLING LOCATION H.S.D.C. - TEST CAR
 SAMPLE TYPE (BAG, INTEGRATED, CONTINUOUS GRAB) INTEGRATED
 ANALYTICAL METHOD ORSAT
 AMBIENT TEMPERATURE 25°C
 OPERATOR B. D. R. G.

COMMENTS:

RUN GAS	1		2		3		AVERAGE NET VOLUME	MULTIPLIER	MOLECULAR WEIGHT OF STACK GAS (DRY BASIS) M _g , lb/lb-mole
	ACTUAL READING	NET	ACTUAL READING	NET	ACTUAL READING	NET			
CO ₂	2.0	2.0	2.0	2.0	2.0	2.0	2.0	44/100	0.88
O ₂ (NET IS ACTUAL O ₂ READING MINUS ACTUAL CO ₂ READING)	20.2	18.2	20.2	18.2	20.2	18.2	18.2	32/100	5.824
CO (NET IS ACTUAL CO READING MINUS ACTUAL O ₂ READING)	20.4	0.2	20.4	0.2	20.4	0.2	0.2	28/100	0.056
N ₂ (NET IS 100 MINUS ACTUAL CO READING)	100	79.6		79.6		79.6	79.6	28/100	22.288
TOTAL									29.048

Plant U.S.S. Clairton
 Date 12-6-84
 Sample Location HQRC-TEST CELL
 Sample Type M-5
 Run Number 7.2
 Operator JARMAN/Smith
 Ambient Temperature ~ 30°F
 Barometric Pressure 29.01 @ 12:25P
 Static Pressure, (H₂O) _____
 Filter Number(s) BA 1035-046

Leak Check: Initial at 17 " Hg, .002 CFM
 Final at 16 " Hg, .002 CFM
 Pilot Leak Check: OK

Impinger Volumes
 Initial Final
 A 100.0 338.0 Net Gain 238
100.0 238.0 138
0 0 0
 B 100.0 108.0 8
100.0 100.0 0
0 0 0
 Silica Gel
691.4 696.4
243.5 252.2

SASS Condensate
N/A
 Total Volume _____

Probe Length and Type 5' TFL
 Nozzle Size & I.D. .301"
 Pitot Coefficient & I.D. .81
 Assumed Moisture _____
 Molecular Weight, Dry, (M_d) _____
 Meter Box Number APT 12
 Meter Coefficient _____
 α Factor _____
 K = _____
 $K(N_d)^4 = \frac{1}{x} \times (\frac{1}{T_s})^4$ _____
 $ΔH = K(N_d)^4 (\frac{T_m}{T_s}) (P)$ _____

Purge - 8.7 to 18.7
 PH - 2.5

Traverse Point Number	MIN:SEC	Gas Meter Reading (V _m), ft ³	Velocity Head (ΔP _v), in. H ₂ O	ROTAMETER		Temperature of					Pump Vacuum In. Hg	Avg. ΔP	Δ H
				Desired	Actual	PUSH STACK TRAVEL	Probe	Impinger	FILTER TEMP	Oven	Gas Meter In Out		
1-4	<u>1:43</u>	Intt. <u>321.875</u> 322.55	.60	18.7	16.0	162	271	40 40		266	41 41	3	.37
	<u>1:41</u>	322.840	.20	9.8	.11AH	162	269	40 40		269	42 41	1	.11
1-5	<u>1:46</u>	323.44	.45	14.5	13.7	156	270	40 40		265	42 42	2	.30
	<u>1:46</u>	323.718	.15	.11AH	.08AH	163	269	40 40		262	42 41	1	.08
1-4	<u>1:48</u>	324.35	.50	13.7	14.5	157	266	40 40		264	43 42	3	.30
	<u>1:58</u>	324.60	.15	.11AH	.08AH	163	269	40 40		265	44 42	1	.08
1-3	<u>1:45</u>	325.39		18.7	16.7	157	265	40 40		266	44 43	3	.39
	<u>1:41</u>	325.674		.11AH	.11AH	165	267	40 40		264	44 43	1	.11
AVG.													

REMARKS: Δ Desired Rotu readings are used as a reference used for today's test.

Traverse Point Number	MIN : SEC Sampling Time, min	Gas Meter Reading (V _m), ft ³	Velocity Head (AP ₁), in. H ₂ O	ROTCMETER		Temperature of						Pump Vacuum in. Hg	Avg. ΔP	Δ H
				Desired	Actual	PUSH STACK TRAVEL	Probe	Igniter	FILTER TEMP	Oven	Gas Meter In Out			
		Init. 325.694		21.1	20.5	16.5	264	40		266	45	5		.53
1-2	:46	326.55	.95	9.8	9.8	166	268	40		266	45	1		.16
1-1	:47	328.03	1.9	29.6	27.0	164	265	40		268	46	7		.75
	:57	328.87	.40	13.8	12.8	164	266	40		267	46	2		.27
2-6	:43	329.63	1.4	24.2	25.2	165	267	40		268	46	7		.75
	:41	330.145	.35	11.9	11.9	163	268	40		265	47	NA		.22
2-5	:45	331.05	1.2	23.2	23.0	159	266	40		260	47	5		.65
	:49	331.592	.30	10.9	10.9	164	267	40		263	47	1		.22
2-4	:46	332.48	1.0	25.2	21.1	155	265	40		263	48	6		.50
	:55	333.145	.40	12.8	12.8	162	265	40		263	48	1		.25
2-3	:45	334.10	1.6	24.2	27.0	163	265	40		260	48	7		.78
	:40	334.628	.45	11.9	13.7	162	265	40		260	48	NA		.28
2-2	:46	335.61	1.6	25.2	27.0	158	264	40		264	48	7		.77
	:49	336.317	.40	14.5	12.8	162	264	40		267	49	2		.26
2-1	:46	337.27	1.3	27.9	24.2	169	264	40		264	48	6.5		.73
	:56	338.054	.55	12.8	15.3	166	270	40		265	49	3		.36
AUG.														

Run No. 7.7 7.2 Date 12-6-84 Sampling Location HCRS TEST CAR

Comments: U could not pull desired rate of 29.6

Traverse Point Number	MIN:SEC Sampling Time, min	Gas Meter Reading (V _g), ft ³ Init. 338.054	Velocity Head (AP ₁), in. H ₂ O	ROTCOMETER		Temperature of					Pump Vacuum in. Hg	Avg. ΔP	Δ H
				Desired	Actual	Push STACK TRAVEL	Probe	Impinger	FILTER TEMP	Oven			
3-6	:47	339.05	1.6	27.0	1.6	158	270	40		267	49	48	76
	:39	339.510	.35	11.9	.35	160	269	40		269	47	47	35
3-5	:44	340.42	1.1	27.0	22.2	158	268	40		262	49	48	64
	:49	340.958	.35	10.9	11.9	161	270	40		261	49	48	24
3-4	:46	341.74	.95	20.5	20.5	172	265	40		262	50	48	48
	:57	342.193	.25	7.8	9.8	167	266	40		265	50	48	13
3-3	:46	342.45	.80	18.7	18.7	159	265	40		266	49	48	45
	:45	343.28	.25	11.0H	9.8	160	268	40		269	50	48	12
3-2	:44	344.06	.75	20.5	20.5	157	265	40		266	50	48	55
	:49	344.480	.25	7.8	9.8	163	266	40		265	50	47	15
3-1	:47	345.37	1.2	22.2	23.2	156	261	40		269	50	48	57
	:57	346.030	.30	9.8	10.9	172	267	40		270	50	48	20
4-6	:46	346.69	.55	18.7	15.3	154	268	40		269	50	49	35
	:42	346.865	.15	7.8	.08	159	270	40		268	50	49	8
4-5	:47	347.44	.40	15.3	12.8	154	266	40		263	50	49	24
	:45	347.580	.10	.08AH	.00AH	159	269	40		263	50	49	05
AUG.													

Run No. 7.2

Date 12-6-84

Sampling Location

HCBC test car

Comments:

[illegible]

Run No. _____

Date 12-6-84

Sampling Location	HCQC test car

Comments: $\Downarrow$ High vacuum due to H_2O in 1st imp. train A
impinger is getting full, carries over

DATE - 12-6-84

RUN# - 7-2

PLANT - USS - CLAIRTON

RAVREE P. IT	OVEN NUMBER	ΔF EXPECTED	ΔP ACTUAL	ROTMETER DESIRED	POINT SAMPLE TIME	COMMENT	Vel. Head in H ₂ O	Rotometer Reading
1.6	A-9	.80 .25	.60 .20	16.0 .114H	1:24		8.05	8.5
1.5	B-9	.50 .20	.50(.45) .15	14.5(13.7) .084H	1:32		8.10	8.2
1.4	C-9	.45 .20	.50 .15	14.5 .084H	1:46		8.15	8.3
1.3	A-11	.80 .20	.75(.65) .20	18.0(16.7) .114H	1:26		8.22	8.5
1.2	B-11	1.0 .25	.95 .25	20.5 9.8	1:35		8.25	8.8
1.1	C-11	1.7 .40	1.9 .40	29.6 12.8	1:44		8.30	10.9
2.6	A-13	1.3 .35	1.4 .35	25.2 11.9	1:26		8.35	11.3
2.5	B-13	1.2 .30	1.2 .30	23.2 10.9	1:34		8.40	11.7
2.4	C-13	1.4 .40	1.0 .40	21.1 12.8	1:41		8.45	12.0
2.3	A-15	1.3 .35	1.6 .45	27.0 13.7	1:25		8.50	12.3
2.2	B-15	1.4 .50	1.6 .40	27.0 12.8	1:35		8.55	12.5
2.1	C-15	1.7 .40	1.3 .55	24.2 15.3	1:42		8.60	12.8
3.6	A-17	1.6 .35	1.6 .35	27.0 13.7	1:26		8.65	13.0
3.5	B-17	1.6 .30	1.1 .35	22.2 11.9	1:33		8.70	13.2
3.4	C-17	.95 .25	.95 .25	20.5 9.8	1:43		8.75	13.4
3.3	A-19	.80 .20	.80 .25	18.7 9.8	1:31		8.80	13.6
3.2	B-19	.95 .25	.95 .25	20.5 9.8	1:33		8.85	13.8
3.1	C-19	1.1 .25	1.2 .30	23.2 10.9	1:44		8.90	14.0
4.6	A-21	.80 .25	.55 .15	15.3 .084H	1:28		8.95	14.2
4.5	B-21	.55 .15	.40 .10	12.8 .054H	1:32		9.00	14.4
4.4	C-21	.80 .25	.65 .15	16.7 .084H	1:43		9.05	14.6
4.3	A-23	1.5 .30	1.3 .30	24.2 10.9	1:27		9.10	14.8
4.2	B-23	1.5 .30	1.4 .30	25.2 10.9	1:42		9.15	15.0
4.1	C-23	1.2 .25	1.3 .25	24.2 9.8	1:44		9.20	15.2
Avq.				TOTAL TIME				

DRY MOLECULAR WEIGHT DETERMINATION

PLANT VSS-CLARK
 DATE 12-6-84 TEST 7.2
 SAMPLING TIME (24 hr CLOCK) _____
 SAMPLING LOCATION H.S.Q.C. - TEST CAR
 SAMPLE TYPE (BAG, INTEGRATED, CONTINUOUS GRAB) INTEGRATED
 ANALYTICAL METHOD ORSAT
 AMBIENT TEMPERATURE 23°C ~ 3:30P
 OPERATOR B. Barlow

COMMENTS:

RUN GAS	1		2		3		AVERAGE NET VOLUME	MULTIPLIER	MOLECULAR WEIGHT OF STACK GAS (DRY BASIS) M _G , lb/lb-mole
	ACTUAL READING	NET	ACTUAL READING	NET	ACTUAL READING	NET			
CO ₂	2.2	2.2	2.2	2.2	2.2	2.2	2.2	44/100	0.968
O ₂ (NET IS ACTUAL O ₂ READING MINUS ACTUAL CO ₂ READING)	19.6	17.4	19.4	17.2	19.4	17.2	17.266	32/100	5.525
CO (NET IS ACTUAL CO READING MINUS ACTUAL O ₂ READING)	19.8	0.2	19.8	0.4	19.8	0.7	0.33	28/100	0.093
N ₂ (NET IS 100 MINUS ACTUAL CO READING)	100	80.2	100	80.2	100	80.2	80.20	28/100	22.456
TOTAL									29.042

Plant VSS-C-AIRTEL, PA
Date 12-13-84
Sample Location HEQS-TEST CAR
Sample Type M-5
Run Number 7.3 (Blank)
Operator TARMAN/milburn
Ambient Temperature _____
Barometric Pressure _____
Static Pressure, (H₂O) _____
Filter Number(s) LA126-047

Leak Check: Initial at 20 = Hg. 0.000 CFM
Final at 15 = Hg. 0.000 CFM
Pitot Leak Check: OK

Impinger Volume	Initial	Final	Net Gain
TRAIN A	100	100.0	
	100	100.0	
	M/I	0	
TRAIN B	100	100.0	
	100	100.0	
	M/I	0	
Silica Gel			
	666.0	673.4	7.4
	659.0	662.0	3.4
SASS Condensate			W/A
Total Volume			

Probe Length and Type 5' TFE
 Nozzle Size & I.D. 0.502 (302)
 Pilot Coefficient & I.D. _____
 Assumed Moisture _____
 Molecular Weight, Dry, (M_d) _____
 Meter Box Number API 12 16
 Meter Coefficient _____
 α Factor _____
 $K = \frac{K(KND)^4}{K(KND)^4} = \frac{K(\quad)^4}{K(KND)^4} = \quad$
 $\Delta H = K(M_d)^4 \left(\frac{T_m}{T_s} \right) (P)$

Purge 5.80 to 15.8
P.H. 5.0

[illegible]

Contents:

Plant VSS Claifton PA

Date 12-13-84

Sample Location HCCG test gas

Sample Type m - 5

Run Number 7.4

Operator JARMAN/M. L. BURN

Ambient Temperature 60°F

Barometric Pressure 29.94 @ 12:05P

Static Pressure, (in. Hg) BA 1029-048

Filter Number(s) BA 1029-048

Leak Check: Initial at 16" Hg, .006 CFM

Final at 16" Hg, .003 CFM

Pilot Leak Check: OK

Impinger Volumes

	Initial	Final	Net Gain
A {	<u>100.0</u>	<u>398.0</u>	<u>298</u>
	<u>100.0</u>	<u>101.0</u>	<u>1</u>
	<u>M/T</u>	<u>1.0</u>	<u>1</u>
B {	<u>100.0</u>	<u>138.0</u>	<u>38</u>
	<u>100.0</u>	<u>102.0</u>	<u>2</u>
	<u>M/T</u>	<u>1.0</u>	<u>1</u>
	Silica Gel		
	<u>673.4</u>	<u>678.6</u>	
	<u>662.0</u>	<u>671.8</u>	

SASS Condensate

Total Volume NA

Probe Length and Type S' TFE

Nozzle Size & I.D. 0.302 x 302

Pitot Coefficient & I.D. .84

Assumed Moisture

Molecular Weight, Dry, (M_d)

Meter Box Number APT 12

Meter Coefficient

α Factor

K =

K(Nd)⁴ = x ()⁴ =

ΔH = K(N_d)⁴ (T_m/T_s) (P)

Purge 72.1 to 82.1 CFM

PH 3.0

Traverse Point Number	MIN:SEC	Gas Meter Reading (V _m), ft ³	Velocity Head (a.p.), in. H ₂ O	ROTO METER		Temperature of						Pump Vacuum in. Hg	Avg. Δ H
				Desired	Actual	Probe	Imp Inqer	Filter Temp	Oven	Gas Meter In	Gas Meter Out		
1-6	45	356.07	1.0	18.7	21.1	NA	265	67	67	268	66	65	.50
	44	356.675	.40	14.5 12.8	12.8	160	270	65	65	269	66	64	.23
1-5	47	357.29	.60	14.5	16.0	158	265	67	67	268	67	65	NA
	56	357.716	.15	11.0H	.84H	161	268	62	62	268	68	66	.08
1-4	46	358.32	.65	13.7	16.7	159	263	68	68	267	68	67	.33
	32	358.620	.20	11.0H	.110H	161	266	66	66	269	69	67	.11
1-3	43	359.35	.95	18.7	20.5	159	264	68	68	267	69	68	.50
	43	359.765	.35	11.0H	11.9	161	268	64	63	264	68	68	.16
Avg.													

Desired Rotometer reading is used as a reference

Comments:

Traverse Point Number	MIN: SEC Sampling Time, min	Gas Meter Reading (V _m), ft ³ Init. 371.065	Velocity Head (AP ₁), in. H ₂ O	ROTAMETER		Temperature of								Pump Vacuum in. Hg	Avg. dP	Δ H
				Desired	Actual	PUSH STICK TRAVEL	Probe	Impinger A	FILTER TEMP	Oven	Gas Meter					
											In	Out				
3-6	:46	372.104	1.2	27.0	23.2	163	263	65	65	269	73	71	5		.64	
	:46	372.587	.40	11.9	12.8	163	267	59	59	268	73	71	1		.20	
3-5	:44	373.47	1.1	27.0	22.2	161	264	66	66	261	73	72	5		.60	
	:55	374.124	.35	11.9	11.8	160	267	60	60	262	73	72	1		.20	
3-4	:44	374.95	1.0	20.5	21.1	158	263	67	66	260	73	72	3.5		.54	
	:38	375.345	.30	9.8	10.9	157	269	60	60	262	73	71	1		.16	
3-3	:44	376.23	.90	18.7	20.0	164	263	67	67	260	74	73	N/A		.65	
	:49	376.262	.27	11.0H	10.5	161	267	60	60	259	74	72	1		.26	
3-2	:44	377.74	1.0	20.5	21.1	162	263	67	67	262	74	73	4		.65	
	:56	378.486	.35	9.8	11.9	162	264	60	60	263	74	73	2		.26	
3-1	:44	379.47	1.45	22.2	25.7	158	262	67	67	266	74	73	5		.78	
	:41	380.157	.45	4.8	12.7	160	266	60	60	268	75	73	2		.35	
4-6	:43	381.05	.75	18.7	18.0	158	265	66	66	269	74	73	4		.61	
	:47	381.679	.25	9.8	9.8	160	269	59	59	269	74	73	1		.24	
4-5	:44	382.46	.50	15.3	14.4	171	264	67	67	264	74	73	3		.42	
	:58	383.140	.15	.084H	.084H	163	265	61	61	263	75	73	1		.0P	
AUG.																

Run No. 2.5 7.4

Date 12-12-84
12-13-84

Sampling Location HCRC - TEST LAB

Comments:

[illegible]

Run No. 77 pg. 24

Q2
one 12-12-84
12-13-84

Sampling Location HCQC-TEST CHL

Static Post - . 07
travel - . 05

Comment:

DATE - 10/10/1954

RUN # - 7.4

PLANT - USS - CLAIRTON

RAVISE FLIT	OVEN NUMBER	ΔP EXPECTED	ΔP ACTUAL	ROTMETER DESIRED	POINT SAMPLE TIME	COMMENT
1.6	B-1		1.5 1.40	21.1 12.8	1:29	
1.5	C-1		1.60 1.15	16.0 10.84H	1:43	
1.4	A-3		1.65 1.20	16.7 11.0H	1:18	
1.3	B-3		1.95 1.35	20.5 4.1R	1:26	
1.2	C-3		1.10 1.35	22.2 11.8	1:36	
1.1	A-5		2.0 1.65	30.4 16.7	1:25	
2.6	B-5		1.45 1.50	25.7 14.54H	1:29	
2.5	C-5		1.65 1.20	16.7 11.1AH	1:42	
2.4	A-7		1.60 1.40	16.0 12.8	1:26	
2.3	B-7		1.80 1.65	18.0 25.6	1:28	
2.2	C-7		1.5 1.55	26.2 15.3	1:40	
2.1	A-9		2.10 1.70	31.1 17.4	1:23	
3.6	B-9		1.82 1.40	23.2 12.8	1:32	
3.5	C-9		1.10 1.35	22.2 11.8	1:41	
3.4	A-11		1.10 1.30	21.1 10.9	1:22	
3.3	B-11		1.90 1.27	20.0 10.5	1:33	
3.2	C-11		1.10 1.35	21.1 11.9	1:40	
3.1	A-13		1.45 1.45	25.3 13.7	1:25	
4.6	B-13		1.75 1.25	18.0 9.8	1:30	
4.5	C-13		1.50 1.15	14.6 DEATH	1:42	
4.4	A-15		1.95 1.25	20.5 9.8	1:24	
4.3	B-15		1.5 1.45	26.2 13.7	1:38	
4.2	C-15		1.95 1.40	30.0 12.8	1:42	
4.1	A-17		1.50 1.35	26.2 11.8	1:25	
TOTAL				TIME		

0.05	0.10	0.15
0.10	0.15	0.20
0.15	0.20	0.25
0.20	0.25	0.30
0.25	0.30	0.35
0.30	0.35	0.40
0.35	0.40	0.45
0.40	0.45	0.50
0.45	0.50	0.55
0.50	0.55	0.60
0.55	0.60	0.65
0.60	0.65	0.70
0.65	0.70	0.75
0.70	0.75	0.80
0.75	0.80	0.85
0.80	0.85	0.90
0.85	0.90	0.95
0.90	0.95	1.00
0.95	1.00	1.05
1.00	1.05	1.10
1.05	1.10	1.15
1.10	1.15	1.20
1.15	1.20	1.25
1.20	1.25	1.30
1.25	1.30	1.35
1.30	1.35	1.40
1.35	1.40	1.45
1.40	1.45	1.50
1.45	1.50	1.55
1.50	1.55	1.60
1.55	1.60	1.65
1.60	1.65	1.70
1.65	1.70	1.75
1.70	1.75	1.80
1.75	1.80	1.85
1.80	1.85	1.90
1.85	1.90	1.95
1.90	1.95	2.00
1.95	2.00	2.05
2.00	2.05	2.10
2.05	2.10	2.15
2.10	2.15	2.20
2.15	2.20	2.25
2.20	2.25	2.30
2.25	2.30	2.35
2.30	2.35	2.40

DRY MOLECULAR WEIGHT DETERMINATION

PLANT USS-CLARK
 DATE 12-13-84
 SAMPLING TIME (24-hr CLOCK) _____
 SAMPLING LOCATION H.S.G.C. - TEST CAR
 SAMPLE TYPE (BAG, INTEGRATED, CONTINUOUS GRA B) INTEGRATED BAG
 ANALYTICAL METHOD ORSH
 AMBIENT TEMPERATURE 25°C
 OPERATOR B. D. Ray

COMMENTS:

RUN GAS	1			2			3			AVERAGE NET VOLUME	MULTIPLIER	MOLECULAR WEIGHT OF STACK GAS (DRY BASIS) M _d , lb/lb-mole
	ACTUAL READING	NET		ACTUAL READING	NET		ACTUAL READING	NET				
CO ₂	1.8			2.2			2.2				44/100	
O ₂ (NET IS ACTUAL O ₂ READING MINUS ACTUAL CO ₂ READING)	20.2			20.4			20.4				32/100	
CO (NET IS ACTUAL CO READING MINUS ACTUAL O ₂ READING)	20.2			20.4			20.4				28/100	
N ₂ (NET IS 100 MINUS ACTUAL CO READING)	100			100			100				28/100	
TOTAL												

Plant DES-C4 AIR TREN PADate 12-14-84Sample Location HCGG-TEST CARSample Type M-5Run Number 2.5Operator JRM/mw/milburnAmbient Temperature ~35°FBarometric Pressure 27.50 (11.25)Static Pressure, (H₂O)Filter Number(s) RA026-047

Impinger Volumes

	Initial	Final	Net Gain
TRAIN A	100	412	312
A	100	114	14
	M/I	M/I	0
TRAIN B	100	120	20
B	100	100	0
	M/I	M/I	0

Silica Gel

A	64.0g	64.65g	5.5g
	654.0g	664.0g	10.0g

Leak Check: Initial at 18 Hg., 001 CFMFinal at 14 Hg., 001 CFMPilot Leak Check: OKSASS Condensate N/A

Total Volume

Probe Length and Type 5' TFE linedNozzle Size & I.D. 302 (302)Pitot Coefficient & I.D. .84

Assumed Moisture

Molecular Weight, Dry, (M_d)Meter Box Number APT 12 LG

Meter Coefficient

α Factor

K =

K(N_d)⁴ = x ()⁴ = ΔH = K(N_d)⁴ () (P)Purge - 82.5-92.5 CFMPH = 2.55

Traverse Point Number	MIN:SEC	Sampling Time, min	Gas Meter Reading (V _m), ft ³	Velocity head (ΔP), in. H ₂ O	Rotameter		Temperature of						Pump Vacuum In. Hg	Avg. Δ H			
					Desired	Actual	PSH	ST	T _W	Probe	Impinger				Oven	Gas Meter	
											A	B				In	Out
1-6	1:01	1:45	Init. 393.111 393.97	.90	20.5	20.5	157	157	54	55	20.5	267	53	52	NA	.57	
	1:01		394.674	.35	11.9	11.9	160	160	50	50	11.9	268	54	52	1	.25	
1-5	1:44	1:44	395.36	.60	16.0	16.0	163	163	55	55	16.0	260	54	54	NA	.42	
	1:44		395.564	.20	0.84H	0.84H	163	163	51	51	11.0H	261	55	53	1	.11	
1-4	1:53	1:46	396.37	.70	16.7	16.7	157	157	55	55	17.4	261	56	54	4	.54	
	1:53		396.800	.15	11.4H	11.4H	162	162	50	50	0.84H	261	56	54	1	.08	
1-3	1:45	1:45	397.64	.90	20.5	20.5	157	157	56	55	20.0	263	56	55	4	.35	
	1:54		398.216	.25	11.9	11.9	162	162	50	50	9.8	259	57	55	1	.17	
Avg.																	

Comments:

Traverse Point Number	MIN:SEC Sampling Time, min	Gas Meter Reading (V _m), ft ³	Velocity Head (AP ₃), in. H ₂ O	ROTOMETER			Temperature of					Pump Vacuum in. Hg	AVG. ΔP	Δ H
				Desired	Actual	PUSH STACK TRAVEL	Probe	Impinger	FILTER TEMP	Oven	Gas Meter In	Gas Meter Out		
1-2	:44	398.216	1.2	22.2	23.2	159	260	55 54		259	57	56	5	.70
	:44	399.610	.40	11.8	12.8	162	263	50 50		259	58	56	1	.29
1-1	:46	400.61	2.10	31.1	27.0	160	260	57 57		259	58	57	7	.82
	:48	401.403	.55	16.7	15.3	161	261	50 50		264	59	57	2	.34
2-6	:46	402.36	1.35	25.7	23.7	173	264	56 56		263	59	58	6	.69
	:57	403.112	.40	14.5	12.8	167	265	50 50		260	60	58	2	.29
2-5	:46	404.03	1.10	16.7	22.2	157	262	56 56		259	59	59	5	.69
	:38	404.495	.40	11.4	12.8	158	261	50 50		259	60	60	2	.22
2-4	:46	405.42	1.25	16.0	23.7	159	262	57 56		256	60	59	5	.73
	:53	406.158	.50	12.8	14.5	159	261	50 50		257	60	59	3	.30
2-3	:45	406.900	.60		16.0	159	261	67 57		260	61	60	NA	.38
	:56	407.410	.15	16.7	28.4	160	260	50 50		259	61	60	1	.08
2-2	:44	408.37	1.6	28.6	27.0	160	260	57 57		258	62	60	6.5	.81
	:53	409.019	.40	15.3	12.8	157	260	51 51		262	62	60	2	.24
2-1	:43	409.96	.90		20.0	160	259	58 58		267	63	61	1.3	.51
	:57	410.657	.35	17.4	11.9	160	259	50 50		258	63	61	1	.21
AUG.														

Run No. 7151

Date 12-14-84

Sampling Location HCQC - TEST CAR

Comments: I could not pull actual desired rate of 31.1

Traverse Point Number	MIN: SEC Sampling Time, min	Gas Meter Reading (V _m), ft ³ Init. 410.657	Velocity Head (AP ₁), in. H ₂ O	ROTOMETER		Temperature of					Pump Vacuum in. Hg	Avg. ΔP	Δ H
				Desired	Actual	PUSH STACK TRAVEL	Probe	Inletings	FILTER TEMP	Oven	Gas Meter In	Gas Meter Out	
3-4	:45	411.55	1.40	23.2	25.2	155	264	58		268	63	62	.79
	:45	412.047	.40	12.8	12.8	152	265	50		267	64	62	.22
3-5	:43	412.90	1.3	22.2	24.2	163	263	58		259	64	62	.74
	:56	413.025	.45	11.8	13.7	157	265	50		262	64	62	.26
3-4	:44	414.43	.95	21.1	20.5	156	262	59		259	64	63	.53
	1:00	415.043	.30	10.9	10.9	155	264	50		260	64	63	.20
3-3	:44	415.80	.80	20.0	18.7	157	261	59		259	65	64	.51
	:50	416.300	.25	10.5	9.8	162	264	51		259	65	64	.17
3-2	:44	417.05	.96	21.1	20.5	152	261	60		256	65	64	.55
	:50	417.653	.13	10.9	10.9	158	262	52		257	66	64	.22
3-1	:43	418.49	1.3		24.2	157	260	60		262	65	66	.73
	:59	419.232	.39		11.8	158	261	52		263	66	65	.24
4-6	:45	419.99	.75	18.0	18.0	152	264	61		260	66	65	.49
	:46	420.369	.25	9.8	9.8	156	266	54		268	67	66	.15
4-5	:44	420.97	.40	14.6	12.8	150	262	61		258	67	66	.27
	:56	421.325	.15	.082H	.082H	155	263	54		261	67	66	.08
AUG.													

Run No. 725 Date 12-14-84 Sampling Location HCCG-TEST CAC

Comments: 11 Lower stack temp than ~~normal~~ normal

COMMENTS:

DATE - 12-15-64

RUN # - 7.5

PLANT - USS - CLAIRTON

RAVERSE POINT	OVEN NUMBER	ΔP EXPECTED	ΔP ACTUAL	ROTMETER DESIRED	POINT SAMPLE TIME	COMMENT
1.6			6.90	20.8	1:46	
1.5	A-17		6.60	11.9	1:28	
1.4	B-17		17.0	11.1AH	1:34	
1.3	C-17		15	10.8AH		
1.2	A-17		12	20.0	1:44	
1.1	B-17		14.0	23.2	1:28	
2.6	C-19		2.10	12.8	1:34	
2.5	A-21		1.25	31.1	1:34	
2.4	B-21		1.40	15.3		
2.3	C-21		1.25	23.7	1:43	
2.2	A-23		1.40	12.8	1:24	
2.1	C-23		1.25	23.7	1:39	
3.6	A-25		1.60	14.5	1:39	
3.5	C-25		1.15	16.0	1:41	
3.4	A-27		1.40	27.0	1:37	WATER in sight A-23
3.3	B-27		1.35	12.5		
3.2	C-27		1.45	20.0	1:40	
4.6	A-29		1.40	11.9	1:30	
4.5	B-29		1.3	25.2	1:30	
4.4	C-29		1.45	12.8	1:39	
4.3	A-2		1.95	13.7	1:39	
4.2	B-2		1.30	20.5	1:46	
4.1	C-2		1.45	10.9	1:34	
4.0	A-2		1.45	9.8	1:34	
3.9	B-2		1.45	10.9	1:40	
3.8	C-2		1.45	10.9	1:40	
3.7	A-2		1.45	10.9	1:40	
3.6	B-2		1.45	10.9	1:40	
3.5	C-2		1.45	10.9	1:40	
3.4	A-2		1.45	10.9	1:40	
3.3	B-2		1.45	10.9	1:40	
3.2	C-2		1.45	10.9	1:40	
3.1	A-2		1.45	10.9	1:40	
3.0	B-2		1.45	10.9	1:40	
2.9	C-2		1.45	10.9	1:40	
2.8	A-2		1.45	10.9	1:40	
2.7	B-2		1.45	10.9	1:40	
2.6	C-2		1.45	10.9	1:40	
2.5	A-2		1.45	10.9	1:40	
2.4	B-2		1.45	10.9	1:40	
2.3	C-2		1.45	10.9	1:40	
2.2	A-2		1.45	10.9	1:40	
2.1	B-2		1.45	10.9	1:40	
2.0	C-2		1.45	10.9	1:40	
1.9	A-2		1.45	10.9	1:40	
1.8	B-2		1.45	10.9	1:40	
1.7	C-2		1.45	10.9	1:40	
1.6	A-2		1.45	10.9	1:40	
1.5	B-2		1.45	10.9	1:40	
1.4	C-2		1.45	10.9	1:40	
1.3	A-2		1.45	10.9	1:40	
1.2	B-2		1.45	10.9	1:40	
1.1	C-2		1.45	10.9	1:40	
1.0	A-2		1.45	10.9	1:40	
0.9	B-2		1.45	10.9	1:40	
0.8	C-2		1.45	10.9	1:40	
0.7	A-2		1.45	10.9	1:40	
0.6	B-2		1.45	10.9	1:40	
0.5	C-2		1.45	10.9	1:40	
0.4	A-2		1.45	10.9	1:40	
0.3	B-2		1.45	10.9	1:40	
0.2	C-2		1.45	10.9	1:40	
0.1	A-2		1.45	10.9	1:40	
0.0	B-2		1.45	10.9	1:40	
TOTAL TIME						

① No reading taken at
A-23

[illegible]

Sampling Location HCGC-TEST CAR

Date 12-14-87.

Run No. 7.5

Static taken point 3-1
push (-.08)
travel (-.05)

Comments:

[illegible]

7.5

Date 12-14-84.

Sampling Location HCQC-TEST CAR

static taken point 3-1
push (-.08)
tension (-.05)

Comments:

DATE - 2-14-54

RUN # - 7.5

PLANT - USS - CLAIRTON

RAVERSE POIN	OVEN NUMBER	ΔP EXPECTED	ΔP ACTUAL	ROTORMETER DESIRED	POINT SAMPLE TIME	COMMENT
1.6			69.0	20.5	11.4	1:46
1.5	A-17		60	16.0	11.4H	1:28
1.4	B-17		70	17.4	10.8AH	1:34
1.3	C-17		90	20.0	9.8	1:44
1.2	A-17		1.2	23.2	12.8	1:28
1.1	B-17		2.10	31.1	15.3	1:34
2.6	C-17		1.25	23.7	12.8	1:43
2.5	A-21		1.10	22.2	12.8	1:24
2.4	B-21		1.25	23.7	14.5	1:39
2.3	C-21		60	16.0	10.8AH	1:41
2.2	MISSING B-23		1.60	27.0	12.5	1:37
2.1	C-23		90	20.0	11.9	1:40
3.6	A-25		1.4	25.2	12.8	1:30
3.5	C-25		1.3	24.2	13.7	1:39
3.4	C-25		1.45	20.5	10.9	1:46
3.3	A-27		80	18.7	9.8	1:34
3.2	B-27		1.15	20.5	10.9	1:40
3.1	C-27		1.30	24.2	12.6	1:42
4.6	A-29		1.75	18.0	9.8	1:31
4.5	B-29		1.40	12.8	10.8AH	1:40
4.4	A-2		1.45	20.5	10.9	1:24
4.3	B-2		1.1	23.2	10.9	1:32
4	C-2		1.45	25.7	11.4	1:39
4.1			1.4	25.2	13.7	1:27
4.0						
				TOTAL TIME		

① No reading taken at A-23

DRY MOLECULAR WEIGHT DETERMINATION

PLANT USS - CLARK
 DATE 12-14-84
 SAMPLING TIME (24 hr CLOCK) _____
 SAMPLING LOCATION HSCC - TEST CAR
 SAMPLE TYPE (BAG, INTEGRATED, CONTINUOUS GRAB) INTEGRATED
 ANALYTICAL METHOD ORSAT
 AMBIENT TEMPERATURE 25°C
 OPERATOR B. D. Ray

COMMENTS:

RUN GAS	1		2		3		AVERAGE NET VOLUME	MULTIPLIER	MOLECULAR WEIGHT OF STACK GAS (DRY BASIS) M_d , lb/lb-mole
	ACTUAL READING	NET	ACTUAL READING	NET	ACTUAL READING	NET			
CO ₂	2.0	2.0	2.0	2.0	2.0	2.0		44/100	
O ₂ (NET IS ACTUAL O ₂ READING MINUS ACTUAL CO ₂ READING)	20.0	18.0	20.0	18.0	20.0	18.0		32/100	
CO (NET IS ACTUAL CO READING MINUS ACTUAL O ₂ READING)	20.0	0	20.0	0	20.0	0		28/100	
N ₂ (NET IS 100 MINUS ACTUAL CO READING)	100	80.0	100	80.0	100	80.0		28/100	
TOTAL									

Plant ISS-CLAIRTON, PA
 Date 10-15-87
 Sample Location H.C.O.C. - TEST CAR
 Sample Type M-5
 Run Number 3.1
 Operator JARMAN/SMITH
 Ambient Temperature 78.0 F
 Barometric Pressure 30.75 1145 hPa
 Static Pressure, (H₂O) 1.75 T = .20
 Filter Number(s) RA1026-017
RA1026-022

Leak Check: Initial at 16 " Hg. 0.00 CFM
 Final at 15 " Hg. 0.01 CFM
 Pitot Leak Check: OK

Impinger Volumes
 Initial Final
 Imp A1 100 284.0
2 100 300
3 0 0
 Imp B1 100 236.0
2 100 102.2
3 0 0
 Silica Gel
658.7 666.5
659.2 666.9
 SASS Condensate N/A
 Total Volume 537.7

Probe Length and Type 5' TFE LINED
 Nozzle Size & I.O. 1.302 in
 Pitot Coefficient & I.O. 0.84
 Assumed Moisture ~ 31%
 Molecular Weight, Dry, (M_d)
 Meter Box Number APT 12 LG 1100
 Meter Coefficient
 α Factor
 $K =$
 $K(M_d)^4 = \frac{1}{x} \left(\frac{1}{T_s} \right)^4$
 $\Delta H = K(M_d)^4 \left(\frac{1}{T_s} \right) (P)$

pt - 3.5

Traverse Point Number	MIN:SEC	Gas Meter Reading (V _m), ft ³	Velocity Head (ΔP), in. H ₂ O	ROTOMETER		PUSH STACK TRAVEL	Probe	Temperature of				Pump Vacuum in. Hg	Avg. Δ H
				Desired	Actual			Impinger	Filter Temp	Oven	Gas Meter In Out		
1-6	<u>.49</u>	Init. <u>752.570</u> <u>753.340</u>	<u>.83</u>		<u>19.3</u>	<u>157</u>	<u>276</u>	<u>80</u>	<u>247</u>	<u>244</u>	<u>72</u> <u>72</u>	<u>3</u>	<u>.43</u>
1-5	<u>1:02</u>	<u>753.929</u>	<u>.20</u>		<u>.114H</u>	<u>163</u>	<u>275</u>	<u>68</u>	<u>290</u>	<u>248</u>	<u>72</u> <u>71</u>	<u>1</u>	<u>.11</u>
	<u>.43</u>	<u>754.601</u>			<u>19.5</u>	<u>155</u>	<u>274</u>	<u>80</u>	<u>298</u>	<u>245</u>	<u>75</u> <u>73</u>	<u>2</u>	<u>.30</u>
1-4	<u>.51</u>	<u>755.558</u>			<u>.084H</u>	<u>159</u>	<u>273</u>	<u>66</u>	<u>296</u>	<u>256</u>	<u>75</u> <u>73</u>	<u>1</u>	<u>.84H</u>
	<u>.49</u>	<u>755.923</u>		<u>15.3</u>	<u>15.3</u>	<u>153</u>	<u>274</u>	<u>80</u>	<u>305</u>	<u>249</u>	<u>77</u> <u>75</u>	<u>NA</u>	<u>.32</u>
1-3	<u>.49</u>	<u>756.741</u>	<u>.95</u>	<u>.084H</u>	<u>20.5</u>	<u>157</u>	<u>276</u>	<u>68</u>	<u>299</u>	<u>258</u>	<u>78</u> <u>76</u>	<u>NA</u>	<u>.084H</u>
	<u>.43</u>	<u>757.171</u>	<u>.25</u>		<u>20.5</u>	<u>155</u>	<u>273</u>	<u>80</u>	<u>303</u>	<u>246</u>	<u>77</u> <u>77</u>	<u>NA</u>	<u>NA</u>
Avg.					<u>9.8</u>	<u>158</u>	<u>276</u>	<u>68</u>	<u>298</u>	<u>253</u>	<u>81</u> <u>80</u>	<u>1</u>	<u>NA</u>

Comments:

Traverse Point Number	MIN:SEC Sampling Time, min	Gas Meter Reading (V _m), ft ³	Velocity Head (h _{ps}), in. H ₂ O	ROTOMETER		Temperature of					Pump Vacuum in. Hg	Avg. dip	Δ H
				Desired	Actual	Push Stack Travel	Probe	Impinger	FILTER TEMP	Oven	Gas Meter In	Gas Meter Out	
1-2	:52	758.05	1.01		23.2	156	223	82	309	252	83	82	NA
	:52	758.719	.35		11.9	159	274	64	292	252	85	82	.25
1-1	:50	759.900	2.2		31.9	150	272	84	308	254	86	87	1.1
	:56	760.810	.65		16.7	157	272	60	293	257	87	84	NA
2-6	:49	761.850	1.7		27.9	157	274	84	310	257	87	85	.86
	:35	762.403	.60		16.0	156	272	62	293	261	88	85	.39
2-5	:50	763.41	1.4		25.2	158	274	84	311	256	88	86	.73
	:51	764.108	.45		13.7	158	274	64	289	254	88	86	.27
2-4	:50	765.10	1.4		25.2	153	274	84	311	254	89	87	.71
	1:06	766.756*	.55		15.3	160	270	52	287	287	89	87	.34
2-3	:49	767.08	1.7		32.7	162	273	83	308	253	90	88	.87
	:49	767.848	.60		16.0	159	270	62	285	252	91	88	.38
2-2	:50	769.00	1.8		28.6	157	273	84	308	252	91	90	.95
	:54	769.840	.60		16.0	159	272	62	286	252	91	89	.39
2-1	:50	771.10	2.4		33.4	156	273	84	310	253	91	90	1.1
	1:00	772.095	.75		18.0	169	269	61	284	252	92	89	.40
Avg.													

Run No. 2.1 Date 10-19-84 Sampling Location NCC - Test car

Comments: * Assumed vol reading was 765.996

Traverse Point Number	MIN:SEC Sampling Time, min	Gas Meter Reading (V _m), ft ³ Init. 772.095	Velocity Head (ΔP _s), in. H ₂ O	ROTOMETER		Temperature of						Pump Vacuum in. Hg	Avg. ΔP	Δ H		
				Desired	Actual	Push Stack TRAOEL	Probe	Impinger	FILTER TEMP	Oven	Gas Meter					
											In				Out	
3-6	:47	773.16	1.9		29.6	151	274	84	82	308	252	91	90	7		.97
	:34	773.640	.55		15.3	157	274	62	60	284	260	92	90	2.5		.35
3-5	:48	774.69	1.7		27.9	151	274	84	82	308	252	92	90	7		.91
	:44	775.363	.55		15.3	154	274	64	62	287	256	92	90	2.5		.37
3-4	:48	776.39	1.4		25.2	150	273	84	82	311	234	92	91	5		.15
	:48	776.945	.40		12.8	154	274	64	64	289	259	92	90	2		.26
3-3	:48	777.82	1.0		21.1	153	273	84	82	311	255	92	91	4.5		.57
	:34	778.253	.33		11.9	187	273	66	64	240	253	92	90	2		.23
3-2	:48	779.12	1.2		23.2	152	273	84	82	309	254	93	91	4.5		.60
	:42	779.609	.31		10.7	157	274	64	62	292	253	92	90	NA		.21
3-1	:50	780.68	1.8		28.6	154	273	84	82	310	254	92	92	6.5		.87
	:53	781.475	5.0		14.5	157	272	62	60	292	259	92	90	2.5		.30
4-6	:44	782.43	1.6		27.0	163	273	84	82	312	253	92	91	6		.85
	:37	782.935	.50		14.5	156	270	64	62	296	254	95	95	NA		.29
4-5	:44	783.54	4.3 6.0		16.0	155	274	82 80	80	311	254	92	91	NA		NA
	:48	783.928	7.15		08.04	154	271	62	60	308	256	93	91	NA		NA
AUG.																

Run No. 3.1 Date 10-15-84 Sampling Location HCR C Test Car

Comments: Static 17 20 4-5
-.50 P -.75
-.20 + -.20

[illegible]

Run No. 21 Date 10-19-84 Sampling Location 4000 test car

* Assumed vol reading was 789.70 (calculated from previous readings)

DRY MOLECULAR WEIGHT DETERMINATION

PLANT USS-CLAIRTON
 DATE 10-19-84
 SAMPLING TIME (24-hr CLOCK) _____
 SAMPLING LOCATION HSCC - TEST CAR 3.1
 SAMPLE TYPE (BAG, INTEGRATED, CONTINUOUS GRAB) INTEGRATED BAG
 ANALYTICAL METHOD ORSAT
 AMBIENT TEMPERATURE _____
 OPERATOR B.C. Dabos

COMMENTS:

RUN GAS	1		2		3		AVERAGE NET VOLUME	MULTIPLIER	MOLECULAR WEIGHT OF STACK GAS (DRY BASIS) M _g , lb/lb-mole
	ACTUAL READING	NET	ACTUAL READING	NET	ACTUAL READING	NET			
CO ₂	1.8		1.8		1.8			44/100	
O ₂ (NET IS ACTUAL O ₂ READING MINUS ACTUAL CO ₂ READING)	19.6		21.0		20.4 18.8			32/100	
CO (NET IS ACTUAL CO READING MINUS ACTUAL O ₂ READING)	19.6		21.0		20.4 18.8			28/100	
N ₂ (NET IS 100 MINUS ACTUAL CO READING)	100		100		100			28/100	
TOTAL									

RUN # - 3.1

PLANT - USS - CLAIRTON

AVERAGE POINT	OVEN NUMBER	ΔP EXPECTED	ΔP ACTUAL	ROTOMETER DESIRED	POINT SAMPLE TIME	COMMENT
1.6	K-21	.75	.83	19.3	1:51	.11ΔH
1.5	A-23	.52	.50	14.5	1:35	.08ΔH
1.4	B-23	.53	.55	15.3	1:40	.08ΔH
1.3	A-25	1.2	.95	20.5	1:32	
1.2	B-25	1.6	1.1	22.2	1:44	
1.1	C-25	2.6	2.2	31.9	1:46	
2.6	A-27	1.2	1.7	27.9	1:24	
2.5	B-27	1.2	1.4	25.2	1:41	
2.4	C-27	1.7	1.4	25.2	1:51	
2.3	A-29	2.2	1.7	27.9	1:38	
2.2	B-29	2.1	1.8	28.6	1:44	
2.1	C-29	2.8	2.4	32.7	1:50	
3.6	A-2	1.7	1.9	29.6	1:21	
3.5	B-2	1.7	1.7	27.9	1:32	
3.4	C-2	1.1	1.4	25.2	1:36	
3.3	A-4	1.5	1.0	21.1	1:22	
3.2	B-4	1.2	1.2	23.2	1:30	
3.1	C-4	1.5	1.8	28.6	1:43	
4.6	A-6	1.1	1.6	27.0	1:21	
4.5	B-6	.43	.60	16.0	1:31	.08ΔH
4.4	C-6	1.1	1.3	24.2	1:40	
4.3	A-8	1.7	1.9	29.6	1:22	
4.2	B-8	2.1	2.0	30.4	1:31	
4.1	E-8	1.8	1.7	27.9	1:26	
100.					TOTAL TIME	

Rotometer Reading	Rotometer Reading	Rotometer Reading
3.5	3.7	3.2
3.6	3.8	3.3
3.7	3.9	3.4
3.8	4.0	3.5
3.9	4.1	3.6
4.0	4.2	3.7
4.1	4.3	3.8
4.2	4.4	3.9
4.3	4.5	4.0
4.4	4.6	4.1
4.5	4.7	4.2
4.6	4.8	4.3
4.7	4.9	4.4
4.8	5.0	4.5
4.9	5.1	4.6
5.0	5.2	4.7
5.1	5.3	4.8
5.2	5.4	4.9
5.3	5.5	5.0
5.4	5.6	5.1
5.5	5.7	5.2
5.6	5.8	5.3
5.7	5.9	5.4
5.8	6.0	5.5
5.9	6.1	5.6
6.0	6.2	5.7
6.1	6.3	5.8
6.2	6.4	5.9
6.3	6.5	6.0
6.4	6.6	6.1
6.5	6.7	6.2
6.6	6.8	6.3
6.7	6.9	6.4
6.8	7.0	6.5
6.9	7.1	6.6
7.0	7.2	6.7
7.1	7.3	6.8
7.2	7.4	6.9
7.3	7.5	7.0
7.4	7.6	7.1
7.5	7.7	7.2
7.6	7.8	7.3
7.7	7.9	7.4
7.8	8.0	7.5
7.9	8.1	7.6
8.0	8.2	7.7
8.1	8.3	7.8
8.2	8.4	7.9
8.3	8.5	8.0
8.4	8.6	8.1
8.5	8.7	8.2
8.6	8.8	8.3
8.7	8.9	8.4
8.8	9.0	8.5
8.9	9.1	8.6
9.0	9.2	8.7
9.1	9.3	8.8
9.2	9.4	8.9
9.3	9.5	9.0
9.4	9.6	9.1
9.5	9.7	9.2
9.6	9.8	9.3
9.7	9.9	9.4
9.8	10.0	9.5
9.9	10.1	9.6
10.0	10.2	9.7

FIL DATA

Plant USS - Clinton
 Date 10-21-84
 Sample Location HCCSC - test cell
 Sample Type m-5
 Run Number 3.2
 Operator JARMAN/Smith
 Ambient Temperature ~50°F
 Barometric Pressure 30.41
 Static Pressure, (H₂O) _____
 Filter Number(s) RA102G-021
RA102G-020

Impinger Volumes
 Initial Final
 A 100.0 181.0 Net Gain 184
200.0 262.0 (-42)
 B 100.0 125.0 0
200.0 191.0 38
 C 0 0 1
 D 0 0 0
 Silica Gel
669 613 49
665 614 49
 SASS Condensate NA
 Total Volume _____

Probe Length and Type 5' TFE
 Nozzle Size & I.D. .302"
 Pitot Coefficient & I.D. .84
 Assumed Moisture 31%
 Molecular Weight, Dry, (M_d) _____
 Meter Box Number APT 12
 Meter Coefficient _____
 α Factor _____
 $K = \frac{1}{C} \times \left(\frac{1}{T_3} \right)^4$
 $K(M_d)^4 = \frac{1}{C} \times \left(\frac{1}{T_3} \right)^4$
 $\Delta H = K(M_d)^4 \left(\frac{T_m}{T_3} \right) (P)$

PH 3.5

Leak Check: Initial at 15 " Hg, 006 CFM
 Final at 15 " Hg, 010 CFM
 Pitot Leak Check: OK

Traverse Point Number	MIN:SEC	Gas Meter Reading (V _m), ft ³	Velocity Head (ΔP), in. H ₂ O	ROTOMETER		Temperature of					Avg. ΔP	Pump Vacuum in. Hg	Δ H
				Desired	Actual	Probe	Impinger A	Impinger B	Filter Temp	Oven	Gas Meter In	Gas Meter Out	
1-6	:49	815.15	.64	19.3	16.7	156	75	72	304	252	75	74	.38
	:41	815.344	.20	11.1	11.4	168	62	62	304	265	75	74	.11
1-5	:53	816.04	.40	14.5	14.5	153	75	74	316	250	76	75	.30
	:45	816.283	.15	08.4	08.4	159	64	64	299	271	76	75	.08
1-4	:50	816.92	.50	15.3	14.5	151	76	75	323	267	77	76	.25
	:55	816.817.194	.15	08.4	08.4	159	65	64	315	269	77	76	.08
1-3	:49	817.98	.75	20.5	18.0	152	76	76	324	262	77	76	.43
	:40	818.375	.27	9.8	9.8	157	64	63	306	270	78	77	.15
Avg.													

Comments:

Traverse Point Number	MIN:SEC Sampling Time, min	Gas Meter Reading (4), ft ³	Velocity Head (AP ₅), in. H ₂ O	ROTOMETER		Temperature of						Pump Vacuum in. Hg	Avg. ΔP	Δ H
				Desired	Actual	Probe	Impinger	FILTER TEMP	Oven	Gas Meter In	Gas Meter Out			
1-2	:49	818.375	1.2	23.2	23.2	170	78	317	259	78	77	NA		.61
	:54	819.963	.40	11.9	12.8	160	60	303	268	79	78	2		.26
1-1	:51	821.27	2.1	31.9	31.1	154	78	324	266	79	78	NA		1.0
	:53	821.991	.60	16.7	16.0	159	60	299	271	79	77	NA		.36
2-6	:47	822.419	1.2	27.9	23.2	153	78	319	270	80	79	5		.65
	:51	824.075	.50	16.0	14.5	154	60	302	273	81	80	2		.31
2-5	:48	824.91	.80	25.2	21.8	157	78	325	269	81	80	4		.41
	:60	825.602	.40	13.7	12.8	165	60	299	248	82	80	2		.22
2-4	:50	826.182	1.4	25.2	23.2	151	78	320	266	82	81	5		.67
	:42	827.75	.55	13.7	13.7	158	60	299	267	82	80	2		.28
2-3	:50	828.80	1.7	27.9	25.2	167	78	315	263	82	81	6		.83
	:32	829.297	.55	16.0	15.3	162	60	294	269	81	80	NA		NA
2-2	:49	830.44	1.8	28.6	28.6	157	78	315	263	82	81	7		.89
	:47	831.149	.58	16.0	16.0	159	60	290	262	82	81	3		.37
2-1	:51	832.117	2.4	33.4	26.0	165	78	316	259	82	81	NA		NA
	:33	832.705	.85	18.0	17.3	163	62	298	266	82	81	NA		.40
AUG.														

Purge 407.900 to 417.900

Run No. 3-2

Date 10-21-84

Sampling Location

HCRC test car

Comments: 1 Generator died @ 822.417 Repeat Point 2-6
 2 Run 29 to 826.182 Repeat point 2-4
 13 (could not see 20.0 to 4.0 lower emissions)

DRY MOLECULAR WEIGHT DETERMINATION

PLANT USS-CLAIRTON, PA
 DATE 10-22-84
 SAMPLING TIME (24-hr CLOCK) _____
 SAMPLING LOCATION H.C. QC - TEST CAR
 SAMPLE TYPE (BAG, INTEGRATED, CONTINUOUS GRAB) INTEGRATED BAG
 ANALYTICAL METHOD DRY SAT
 AMBIENT TEMPERATURE _____
 OPERATOR B.C. Dales

COMMENTS:

RUN GAS	1		2		3		AVERAGE NET VOLUME	MULTIPLIER	MOLECULAR WEIGHT OF STACK GAS (DRY BASIS) M _d , lb/lb mole
	ACTUAL READING	NET	ACTUAL READING	NET	ACTUAL READING	NET			
CO ₂	2.75	2.75	2.7	2.7	2.7	2.7	2.716	44/100	1.195
O ₂ (NET IS ACTUAL O ₂ READING MINUS ACTUAL CO ₂ READING)	20.0	17.25	20.0	17.3	20.0	17.3	17.28	32/100	5.529
CO (NET IS ACTUAL CO READING MINUS ACTUAL O ₂ READING)	20.2	0.2	20.2	0.2	20.1	0.1	0.166	28/100	0.046
N ₂ (NET IS 100 MINUS ACTUAL CO READING)	100	79.8	100	79.8	100	79.9	79.833	28/100	22.353
TOTAL								29.12	

RUN # - 3.2

PLANT - USS - CLAIRTON

AVERAGE POINT	OVEN NUMBER	ΔP EXPECTED	ΔP ACTUAL	ROTOMETER DESIRED	POINT SAMPLE TIME	COMMENT
1.6	A-24	.83 .20	.64 .20	16.7 SEE COMMENT (14.5)	1:30	.11 ΔH
1.5	B-24	.46 .15	.60 (.45) .15	13.7 (14.5)	1:38	.08 ΔH
1.4	C-24	.50 .15	.50 (.45) .15	13.7 (14.5)	1:45	.08 ΔH
1.3	A-26	.95 .25	.85 (.75) .27	19.3 (18.0) 9.8	1:29	
1.2	B-26	1.2 .35	1.2 .40	23.2 12.8	1:43	
1.1	C-26	2.2 .65	2.1 .60	31.1 16.0	1:44	
2.6	A-28	1.7 .60	1.2 .50	23.2 14.5	1:38	
2.5	C-28	1.4 .45	1.0 (.80) .40	21.1 (18.7) 12.8	1:48	
2.4	B-1	1.4 .55	1.2 (1.2) .45	23.2 13.7	1:32	
2.3	A-3	1.7 .60	1.7 .55	27.9 15.3	1:22	
2.2	B-3	1.8 .60	1.8 .58	28.6 16.0	1:36	
2.1		2.4 .75	2.4 .85	33.4 (30.0) 19.3	1:24	26.0 BEST
3.6		1.9 .55				
3.5		1.7 .55				
3.4		1.4 .40				
3.3		1.0 .33				
3.2		1.2 .31				
3.1		1.8 .50				
4.6		1.6 .50				
4.5		.60 .15				
4.4		1.3 .40				
4.3		1.9 .50				
		2.0 .50				
4.1		1.7 .75				
Avg.					TOTAL TIME	

ROTOMETER DESIRED	POINT SAMPLE TIME	COMMENT
2.5	1:30	2.5
2.6	1:38	2.6
2.7	1:45	2.7
2.8	1:45	2.8
2.9	1:45	2.9
3.0	1:45	3.0
3.1	1:45	3.1
3.2	1:45	3.2
3.3	1:45	3.3
3.4	1:45	3.4
3.5	1:45	3.5
3.6	1:45	3.6
3.7	1:45	3.7
3.8	1:45	3.8
3.9	1:45	3.9
4.0	1:45	4.0
4.1	1:45	4.1
4.2	1:45	4.2
4.3	1:45	4.3
4.4	1:45	4.4
4.5	1:45	4.5
4.6	1:45	4.6
4.7	1:45	4.7
4.8	1:45	4.8
4.9	1:45	4.9
5.0	1:45	5.0
5.1	1:45	5.1
5.2	1:45	5.2
5.3	1:45	5.3
5.4	1:45	5.4
5.5	1:45	5.5
5.6	1:45	5.6
5.7	1:45	5.7
5.8	1:45	5.8
5.9	1:45	5.9
6.0	1:45	6.0
6.1	1:45	6.1
6.2	1:45	6.2
6.3	1:45	6.3
6.4	1:45	6.4
6.5	1:45	6.5
6.6	1:45	6.6
6.7	1:45	6.7
6.8	1:45	6.8
6.9	1:45	6.9
7.0	1:45	7.0
7.1	1:45	7.1
7.2	1:45	7.2
7.3	1:45	7.3
7.4	1:45	7.4
7.5	1:45	7.5
7.6	1:45	7.6
7.7	1:45	7.7
7.8	1:45	7.8
7.9	1:45	7.9
8.0	1:45	8.0
8.1	1:45	8.1
8.2	1:45	8.2
8.3	1:45	8.3
8.4	1:45	8.4
8.5	1:45	8.5
8.6	1:45	8.6
8.7	1:45	8.7
8.8	1:45	8.8
8.9	1:45	8.9
9.0	1:45	9.0
9.1	1:45	9.1
9.2	1:45	9.2
9.3	1:45	9.3
9.4	1:45	9.4
9.5	1:45	9.5
9.6	1:45	9.6
9.7	1:45	9.7
9.8	1:45	9.8
9.9	1:45	9.9
10.0	1:45	10.0

FIL DATA

Plant VSS - Clairton
Date 10-23-84
Sample Location H2O - test car
Sample Type M-S
Run Number 303
Operator JARMAN/Smith
Ambient Temperature 50°F
Barometric Pressure 30.80 @ 1140P
Static Pressure, (H₂O) _____
Filter Number(s) RA102G-025
RA102G-026

Impinger Volumes
Initial Final Net Gain
A { 100.0 399.0 299
100.0 100.0 0
B { 100.0 152.0 52
100.0 101.0 1
0 0 0

PH. : 3.0 A 670.6 676.4 5.8
B 666.8 668.3 4.5

Silica Gel

Probe Length and Type 5' TFE
Nozzle Size & I.D. .302"
Pilot Coefficient & I.D. .84
Assumed Moisture 31%
Molecular Weight, Dry, (M_d) _____
Meter Box Number APT 12
Meter Coefficient _____
α Factor _____
 $K = \frac{K(M_d)^4}{K(M_d)^4} \times \left(\frac{T_m}{T_s} \right)^4 = \frac{K(M_d)^4}{K(M_d)^4} (P)$
 $\Delta H = K(M_d)^4 \left(\frac{T_m}{T_s} \right)^4 (P)$

Leak Check: Initial at 16 " Hg, 006 CFM
Final at 10 " Hg, 005 CFM
Pilot Leak Check: OK

Purge - 96.900 to 106.900

Traverse Point Number	MIN:SEC Sampling Time, min	Gas Meter Reading (V _m), ft ³ Init. 834.663	Velocity Head (ΔP _s), in. H ₂ O	ROTOMETER		Temperature of						Pump Vacuum in. Hg	Avg. Δ H	
				Desired	Actual	PUSH STACK TRAVEL	Probe	Impinger A	Impinger B	FILTER Temp	Oven			Gas Meter In
1-6	:50	835.43	.65	19.3	16.7	153	271	60	331	256	63	62	3	38
	:35	835.711	.20	.114H	.114H	160	274	56	326	257	63	61	1	11
1-5	:48	836.35	.55	14.5	15.3	157	270	60	333	259	63	62	NA	.31
11	:47	836.720	.10	.084H	.054H	162	273	56	321	259	63	62	0	.05
1-4	:49	837.44	.55	15.3	15.3	159	271	60	331	258	63	62	3	.36
	:57	837.896	.15	.084H	.114H	165	272	56	321	259	63	62	0	.11
1-3	:47	838.69	.75	20.5	18.0	154	270	60	331	259	64	63	3.5	.42
12	:46	839.112	.25	9.8	9.8	163	274	56	318	257	65	63	NA	NA
Avg.														

Static pressure taken on Battery 19, Point 1-3 push = Travel PCB Rich: -.26 Travel: -0.8

Comments: 1) We noticed 2 differences from 3-2 & 3-1; Scrubber H₂O is a rusty color now compared to clear before and scrubber H₂O is like warm compared to very hot before.
2) Static pressure inaccurate, nozzle interference on Point 1-3

2084

Traverse Point Number	MIN:SEC Sampling Time, min	Gas Meter Reading (V _m), ft ³ Init. 839.112	Velocity Head (ΔP _s), in. H ₂ O	ROTOMETER		Temperature of							Pump Vacuum in. Hg	Avg. ΔH
				Desired	Actual	PUSH STACK TRAVEL	Probe	Impinger	FILTER TEMP	Oven	Gas Meter			
											In	Out		
1-2	:46	839.97	1.2	23.2	23.2	152	270	60	330	251	64	63	4.5	.65
	:52	840.610	.35	11.9	11.9	160	271	55	319	259	65	63	1	.19
1-1	:48	841.70	1.8	31.9	28.6	140	270	60	329	258	65	64	7	.92
	:55	842.448	.52	16.7	14.5	164	272	54	314	260	65	64	2.5	.31
2-6	:45	843.48	.90	27.9	20.0	155	270	60	331	259	65	64	4	.56
	:38	843.863	.35	16.0	11.9	168	272	54	318	260	65	63	N/A	.23
2-5	:48	844.80	.35	25.0	22.2	152	271	60	331	263	65	64	4.5	.12
	:50	845.415	.35	13.7	11.9	157	272	54	262	264	65	63	1	.23
2-4	:47	846.30	1.1	25.2	22.2	151	270	60	331	262	65	64	4	.12
	:53	846.995	.35	13.7	12.9	157	272	54	291	261	66	65	2	.26
2-3	:46	847.97	1.4	25.2	25.2	151	271	62	300	262	66	65	5	.78
	:42	848.535	.45	15.3	13.7	157	274	55	297	260	66	64	2	.24
2-2	:47	849.54	1.5	28.6	26.2	159	271	62	247	260	67	65	6	.90
	:49	850.176	.45	16.0	13.7	160	272	54	261	261	67	65	N/A	.26
2-1	:48	851.37	2.3	33.4	32.7	159	269	62	291	359	67	65	7	1.1
	:57	852.258	.55	18.0	15.3	159	272	54	289	260	67	65	3	.35
AUG.														

Date 10-23-84

Sampling Location

HCQC test cor.

Run No. 3.3

Comments:

U Temp. of scrubber H₂O has now gotten back to temp. of previous tests. Color is still Rusty. [2] Unexplainable why filter temp drop - oven temp stayed the same.
 [3] Static taken Unit 2-3, Battery 19; Push -.84 travel -.27

3034

Traverse Point Number	MIN:SEC Sampling Time, min	Gas Meter Reading (W _g), ft ³ Init. 852.258	Velocity Head (ΔP _s), in. H ₂ O	ROTOMETER		Temperature of						Pump Vacuum in. Hg	Avg. ΔP	Δ H	
				Desired	Actual	Push Stack Travel	Probe	Impinger	FILTER TEMP	Oven	Gas Meter				
											In				Out
3-6	:48	853.229	1.3	29.6	24.2	153	271	60	239	255	67	66	NA		.74
	:39	853.837	.38	15.3	12.8	157	273	54	238	254	67	65	2		.29
3-5	:48	854.90	1.5	27.9	26.2	155	270	60	228	250	67	66	NA		.81
	:49	855.522	.35	15.3	11.9	158	272	54	240	248	67	65	2		.24
3-4	:49	856.33	2.1 ^{1.0}	25.2	19.3	159	269	60	241	240	67	66	NA		.48
	:56	856.871	1.0 ^{1.0}	12.8	11.04	158	272	54	247	238	67	66	0		.11
3-3	:49	857.70	2.8 ^{1.0}	21.1	20.0	152	272	60	224	261	67	65	3.5		.52
	21:44	858.228	.28	11.9	10.9	159	273	54	246	266	66	65	NA		.22
3-2	:47	859.03	.85	23.2	19.3	154	273	60	262	216	67	65	3.5		.48
	31:47	859.485	.26	10.9	9.8	158	273	56	262	209	67	65	1		.15
3-1	:46	860.47	1.3	28.6	24.2	154	272	60	296	213	66	66	5		.78
	1:01	861.221	.35	14.5	11.9	158	273	52	290	222	67	65	2		.23
4-6	:47	862.12	.96	27.0	20.5	157	273	60	297	234	67	65	NA		.53
	:37	862.482	.27	14.5	9.8	155	274	54	308	242	67	65	1		.16
4-5	:45	863.15	.50	16.0	14.5	154	272	60	358	254	67	66	3		.30
	:47	863.355	.15	0.844	.0844	157	272	56	353	255	67	65	0		
AUG.															

Date 10-23-84

Run No. 3-3

Run No.

Sampling Location HCC Test Car

U Replaced 1 or 2 Heat tapes on Filter - heating ok

Comments: 2) Static measured at point 3-3; 19 battery; Push - 48 Travel - 13

3) H₂O inside oven during maintenance of heater; should dry out and give accurate temp

4) Oven temp back to normal reading

[illegible]

Date 10-23-84

Sampling Location

HCC test co.

3
r

3.3 _____ Date 10-2
 (i) static taken point 4-3, battery 19 Push -.75

travel - .20

Comments:

RUN # - 3.3

PLANT - USS - CLAIRTON

VERSE NT	OVEN NUMBER	ΔP EXPECTED	ΔP ACTUAL	ROTOMETER DESIRED	POINT SAMPLE TIME	COMMENT		rotometer Reading
6	A-17	.83	.20	18.0 (16.7)	1:25	.11 ΔH	S T A T I C	3.5
5	B-17	.40	.55	15.3	1:35	.05 ΔH		5.7
4	C-17	.50	.55	15.3	1:46	.11 ΔH		7.3
3	A-19	.95	.25	19.3 (18.0)	1:33			8.5
2.6	B-19	1.2	.35	23.2	1:38		26 08	10.9
1.1	C-19	2.2	.65	28.6	1:43			12.4
2.6	A-21	1.7	.60	21.1 (20.0)	1:27			12.8
2.5	B-21	1.4	.45	22.2	1:38			13.7
2.4	C-21	1.4	.55	22.2	1:40		84 27	14.5
2.3	A-23	1.7	.60	25.2	1:28			15.3
2.2	B-23	1.8	.60	26.2	1:36			16.7
2.1	C-23	2.4	.75	32.7	1:45			17.4
3.6	A-25	1.9	.55	24.2	1:27		48 13	18.0
3.5	B-25	1.7	.55	26.2	1:37			18.7
3.4	C-25	1.4	.40	21.1 (19.3)	1:45	.11 ΔH		19.3
3.3	A-29	1.0	.33	20.0	1:33			20.0
3.2	B-29	1.2	.31	19.3	1:34		0.5 23	20.5
3.1	C-29	1.8	.50	24.2	1:47			21.1
4.6	A-2	1.6	.50	20.5	1:24			21.7
4.5	B-2	.60	.15	16.7 (14.5)	1:32	.08 ΔH		22.6
4.4	C-2	1.3	.40	21.1	1:37		75 20	23.2
4.3	A-4	1.9	.50	25.2	1:20			23.7
4.2	B-4	2.0	.50	27.0	1:32			24.2
4.1	C-4	1.7	.75	24.2	1:41			24.7
109.					TOTAL TIME			25.2

water from duct
rusty looking & cooler
* = 20 Battery

DRY MOLECULAR WEIGHT DETERMINATION

PLANT USS - CLAIRBORO, PA
 DATE 10-23-84
 SAMPLING TIME (24-hr CLOCK) _____
 SAMPLING LOCATION H.C.Q.C. - TEST CAR 3.3
 SAMPLE TYPE (BAG, INTEGRATED, CONTINUOUS GRAB) INTEGRATED BAG
 ANALYTICAL METHOD ORSAT
 AMBIENT TEMPERATURE _____
 OPERATOR R.C. Dr. Res

COMMENTS:

RUN GAS	1		2		3		AVERAGE NET VOLUME	MULTIPLIER	MOLECULAR WEIGHT OF STACK GAS (DRY BASIS) M _D , lb/lb-mole
	ACTUAL READING	NET	ACTUAL READING	NET	ACTUAL READING	NET			
CO ₂	2.0	2.0	2.0	2.0	2.0	2.0	2.0	44/100	0.88
O ₂ (NET IS ACTUAL O ₂ READING MINUS ACTUAL CO ₂ READING)	21.0	19.0	20.0	18.0	20.0	18.0	18.0	32/100	5.76
CO (NET IS ACTUAL CO READING MINUS ACTUAL O ₂ READING)	21.0	0	20.2	0.2	20.2	0.2	0.2	28/100	0.056
N ₂ (NET IS 100 MINUS ACTUAL CO READING)	100	79	100	79.8	100	79.8	79.8	28/100	22.344
TOTAL									29.04

FILE DATA

Plant USS Clinton
 Date 10-24-84
 Sample Location HSCC test car
 Sample Type M-5
 Run Number 3-4
 Operator JARMAN/SMITH
 Ambient Temperature 30.79 @ 2:00P
 Barometric Pressure (H₂O)
 Static Pressure, (H₂O) RAID26-030
 Filter Number(s) RAID26-031

Leak Check: Initial at 17 " Hg, 006 CFM
 Final at 15 " Hg, 000 CFM
 Pitot Leak Check: OK

Impinger Volumes
 Initial Final
 A { 100.0 381.0
100.0 102.0
 B { 0 0
100.0 128.0
100.0 101.0
0 0
 Net Gain
281
2
0
74
1
0
 Silica Gel
676.4 682.0
663.3 672.2
 SASS Condensate
NA
 Total Volume
376.5

Probe Length and Type 5' TFE
 Nozzle Size & I.D. .302"
 Pilot Coefficient & I.D. .84
 Assumed Moisture 3%
 Molecular Weight, Dry, (M_d)
 Meter Box Number APT 12
 Meter Coefficient
 α Factor
 K =
 $K(M_d)^4 = \text{---} \times (\text{---})^4 = \text{---}$
 $\Delta H = K(M_d)^4 \left(\frac{T_m}{T_s}\right) (P)$

Purge - 419.00 to 429.00 CFM
 P.H. - 3.0

Pilot Leak Check: <u>OK</u>		MIN:SEC		Gas Meter Reading (V _m), ft ³	Velocity Head (ΔP), in. H ₂ O	ROTOMETER			Temperature of						Pump Vacuum in. Hg	Avg. ΔP	Δ H
Traverse Point Number	Sampling Time, min					Desired	Actual	Probe	Impinger	Filter Temp	Oven	Gas Meter					
												In	Out				
1-6	:47		882.09		.65	16.7	16.7	271	60	52	241	56	55	3	NA		
			882.548		.25	.1144	9.8	272	50	50	247	56	55	NA	.16		
1-5	:57		883.12		.52	15.3	14.5	269	60	58	262	57	56	2		.29	
			883.431		.15	.0544	.0844	272	56	54	258	57	56	NA	.28		
1-4	:50		884.08		.50	15.3	14.5	271	60	58	231	58	57	2		.27	
			884.458		.20	.0844	.1144	273	55	54	240	58	58	1		.11	
1-3	:45		885.23		.75	18.0	18.0	270	60	60	290	59	58	4		.39	
			885.781		.25	13.7	9.8	271	50	50	277	62	58	1		.13	
Avg.	1:01																

P.H. - 3.0

21.12

total volume

Comments:

Traverse Point Number	MIN:SEC Sampling Time, min	Gas Meter Reading (V _m), ft ³ Int. 885.78/	Velocity Head (AP ₃), in. H ₂ O	ROTOMETER		Temperature of							Pump Vacuum in. Hg	Avg. Δ H
				Desired	Actual	Push Stack Travel	Probe	Impinger	FILTER TEMP	Oven	Gas Meter			
											In	Out		
1-2	:49	886.69	1.0	23.2	21.1	157	269	60	332	254	61	59	4.5	.57
1-1	:38	887.154	.30	11.9	10.9	161	271	56	282	251	61	59	NA	.22
1-1	:48	888.28	.20	28.6	30.4	154	270	60	343	252	61	60	7	.97
1-1	:53	889.043	.50	14.5	14.5	161	269	54	282	252	62	60	NA	.31
2-6	:47	889.87	1.2	20.0	21.1	155	272	62	269	261	63	62	5	.55
2-5	1:02	890.633	1.1	14.5	11.9	162	276	54	267	260	64	62	2	.24
2-5	:47	891.52	1.1	22.2	22.2	155	270	63	257	256	64	63	5	.61
2-5	:32	891.949	.40	16.0	12.8	163	271	56	244	258	65	63	NA	.25
2-4	:47	892.28	1.3		22.2	157	270	64	333	280	65	64	6	.66
2-4	:41	893.492	.50		11.9	163	270	58	274	258	66	64	NA	.31
2-3	:48	894.50	1.5		25.2	157	268	65	246	253	66	65	NA	.77
2-3	:48	895.153	.45		13.7	160	269	58	235	250	67	65	2	.27
2-2	:48	896.17	1.5		26.2	155	269	65	250	254	67	66	6	.78
2-2	:33	896.625	.45		13.7	160	269	58	244	253	68	65	2	.28
2-1	:47	897.73	2.0		32.7	158	269	65	300	257	68	66	8	1.0
2-1	:41	898.372	.70		15.3	162	268	58	266	254	69	67	3.5	.42
Avg.														

Run No. 3.4

Date 10-24-84

Sampling Location HSCC-TESTLAB

Comments: 11 Changed filter heater controller

Traverse Point Number	MIN:SEC Sampling Time, min	Gas Meter Reading (Vol. ft ³)	Velocity Head (ft H ₂ O)	ROTOMETER		Temperature of					Pump Vacuum In. Hg	Avg. W.P.	Δ H
				Desired	Actual	PUSH STACK TRAVEL	Probe	Impinger	FILTER TEMP	Oven	Gas Meter In Out		
3-6	:48	Intt. 898.372 899.32	1.2	24.2	23.2	153	268	65 63	250	255	68 67	5	.66
	:53	899.953	.40	11.9	12.8	160	268	59 57	258	255	69 67	NA	.23
3-5	:48	900.99	1.6	26.2	27.0	155	271	65 63	320	255	69 68	6.5	.82
	:35	901.467	.45	11.9	13.7	158	270	59 58	253	256	69 67	2	.29
3-4	:47	902.29	.95	19.3	20.5	156	270	64 62	262	264	70 68	4	.55
	:44	902.720	.25	8.6	9.8	160	270	58 58	243	260	70 67	NA	.15
3-3	:48	903.55	.90	20.0	20.0	157	271	65 63	241	270	71 69	4	.50
	:56	904.158	.30	10.9	10.7	158	271	60 58	230	265	70 69	1	.26
3-2	:46	904.92	.85	19.3	19.3	154	270	65 63	278	260	71 69	4	.48
	:36	905.298	.30	9.8	10.9	160	270	60 58	269	258	71 69	NA	NA
3-1	:47	906.19	1.1	24.2	22.2	157	269	65 63	308	252	71 70	5	.62
	:43	906.733	.40	11.9	12.8	160	270	59 57	279	247	71 70	NA	NA
4-6	:49	907.48	.65	20.5	16.7	154	269	65 63	300	252	72 70	3	.38
	:52	907.940	.25	9.8	9.8	156	272	58 56	303	254	71 70	1	.13
4-5	:46	908.59	.60	14.5	16.0	156	270	65 63	320	260	72 70	3	.35
	:38	908.766	.15	.084H	.084H	159	272	60 58	308	262	71 70	NA	.07
AUG.													

Run No. 34

Date 10-24-84

Sampling Location HCLC-TEST CAR

UL Scrubber H₂O is cleaner compared to test 3.4

Comments:

+

8

+

[illegible]

Sampling Location HCC-TESTCAR.

Date 10-24-84

Run No. 3.4

Comments:

324

DRY MOLECULAR WEIGHT DETERMINATION

PLANT USS - CLAIRTON, PA
 DATE 10-24-84
 SAMPLING TIME (24-hr CLOCK) _____
 SAMPLING LOCATION HCO₂ - TEST CAR 3.4
 SAMPLE TYPE (BAG, INTEGRATED, CONTINUOUS GRAB) INTEGRATED BAG
 ANALYTICAL METHOD ORSAT
 AMBIENT TEMPERATURE _____
 OPERATOR B.C. DeRos

COMMENTS:

RUN GAS	1		2		3		AVERAGE NET VOLUME	MULTIPLIER	MOLECULAR WEIGHT OF STACK GAS (DRY BASIS) M _d , lb/lb-mole
	ACTUAL READING	NET	ACTUAL READING	NET	ACTUAL READING	NET			
CO ₂	2.2	2.2	2.2	2.2	2.2	2.2	2.2	44/100	0.968
O ₂ (NET IS ACTUAL O ₂ READING MINUS ACTUAL CO ₂ READING)	20.6	18.4	20.4	18.2	20.6	18.4	18.33	32/100	5.8656
CO (NET IS ACTUAL CO READING MINUS ACTUAL O ₂ READING)	20.9	0.3	20.6	0.4	20.9	0.3	0.333	28/100	0.093
N ₂ (NET IS 100 MINUS ACTUAL CO READING)	100	79.1	100	79.4	100	79.1	79.200	28/100	22.176
TOTAL									29.10

APPENDIX E
DATA REDUCTION

FIELD DATA

Plant	USS - Clairton, PA
Date	12/5/84
Car No.	104
Battery No.	20
Sample Location	HCQC - Test Car
Sample Type	M-5
Run Number	7.1
Operator	Smith/Jarman
No. of Ovens Tested	24
No. of Ovens Tested/hr	3.6
Coke Prd'n Rate, tons/oven	14.5
Ambient Temp, deg F	29
Barometric Pressure, in Hg	29.42
Static Pressure, in H2O	-0.1
Stack Area, ft ²	32.125
Filter Type	RA 934ah
Top Filter Number	RA102G-045
Bottom Filter Number	None
Probe Length & Type	5 ft - TFE Lined
Nozzle Size	0.296
Pitot Coefficient	0.84
Meter Box Number	APT 12 LG Mod
DGM Coeff's A1	0.0012
A2	1.0171
A3	0.0037
Orifice Coeff's B	0.4821
A	0.391
Cal Press, in Hg	29.65

	in Hg	CFM
Leak Check Initial	16	0.004
Final	15	0.004

Water Volume:

Location	Initial	Final	Net Gain
Imp A1	100	356	256
Imp A2	100	140	40
Imp A3	0	1	1
Sil Gel A	687.3	691.4	4.1
Imp B1	100	101	1
Imp B2	100	100	0
Imp B3	0	0	0
Sil Gel B	736	743.5	7.5
Total Volume			309.6

Combined Impinger pH	3.5
----------------------	-----

	Point No.	Oven No.	Start Time	Sample Time		Gas Metr ft3	Rotometer	Orifice del P in. WC
				Total	DGM Start			
						288.474		
P	1.6	C-26	10:28	99	44	289.210	18.7	
T					55	289.737	9.8	0.09
P	1.5	A-28	10:45	88	45	290.310	14.5	0.28
T					43	290.607		0.11
P	1.4	B-28	11:06	93	44	291.150	13.7	0.25
T					49	291.508		0.11
P	1.3	A-1	11:55	83	45	292.300	18.7	0.42
T					38	292.638		0.11
P	1.2	B-1	12:16	92	45	293.313	21.1	0.58
T					47	293.450	9.8	0.13
P	1.1	C-1	12:29	93	47	294.920	29	0.81
T					46	295.530	12.8	0.21
P	2.6	A-3	12:59	76	44	297.651	24	0.70
T					32	298.035	11.9	
P	2.5	B-3	13:12	92	46	298.920	23.2	0.65
T					46	299.468	10.9	0.19
P	2.4	C-3	13:23	98	47	300.430	25.2	0.74
T					51	301.063	12.8	0.26
P	2.3	A-5	13:42	84	47	302.000	24.2	0.70
T					37	302.425	11.9	0.20
P	2.2	B-5	13:55	94	46	303.410	25.2	0.75
T					48	304.050	14.5	0.30
P	2.1	C-5	14:09	99	46	305.040	27	0.80
T					53	305.717	12.8	0.28
P	3.6	A-7	14:22	84	46	306.720	27	0.83
T					38	307.159	11.9	0.21
P	3.5	B-7	14:38	90	45	308.170	27	0.85
T					45	308.720	10.9	0.23
P	3.4	C-7	14:51	105	46	309.540	20.5	0.54
T					59	310.051	9.8	0.13
P	3.3	A-9	15:05	87	46	310.840	18.7	0.46
T					41	311.123		0.11
P	3.2	B-9	15:18	89	44	311.930	20.5	0.55
T					45	312.331	9.8	0.14
P	3.1	C-9	15:31	100	46	313.190	22.2	0.62
T					54	313.674	9.8	0.14
P	4.6	A-11	15:43	88	43	314.370	18.7	0.45
T					45	314.776	9.8	0.13
P	4.5	B-11	15:56	90	45	315.420	15.3	0.33
T					45	315.670		0.08
P	4.4	C-11	16:09	100	43	316.400	18.7	0.47
T					57	316.907	9.8	0.15
P	4.3	A-13	16:21	84	46	317.890	26.2	0.82
T					38	318.344	10.9	0.22
P	4.2	B-13	16:34	92	45	319.270	26.2	0.77
T					47	319.782	10.9	0.19
P	4.1	C-13	16:47	99	45	320.645	23.2	0.67
T					54	321.203	9.8	0.15
Total (Time in minutes)				36.65	32.729			
Push				18.10	21.800	File: DAT		701
Travel				18.55	10.929	Page 2 of 8		

	Point No.	Temperature, deg F						
		Stack	Probe	Oven	Imping A	Imping B	GM In	GM Out
P	1.6	164	271	270	37	38	37	37
T		158	272	273	35	35	38	37
P	1.5	154	266	266	38	38	39	38
T		157	269	271	38	39	39	38
P	1.4	156	266	267	38	38	40	39
T		158	269	267	38	39	41	39
P	1.3	157	266	266	40	40	43	43
T		161	269	267	40	40	44	42
P	1.2	156	265	267	40	40	44	43
T		156	269	265	39	39	45	43
P	1.1	159	265	266	40	40	45	44
T		162	263	268	40	40	45	43
P	2.6	155	268	265	40	40	45	44
T		159	270	268	39	40	46	44
P	2.5	155	268	263	40	40	45	45
T		158	270	266	40	40	46	44
P	2.4	152	268	260	40	40	46	45
T		160	270	262	39	39	46	44
P	2.3	154	267	262	40	40	46	45
T		159	268	269	39	39	46	44
P	2.2	156	266	270	40	40	46	45
T		159	268	270	40	40	46	45
P	2.1	156	266	270	40	40	46	46
T		158	267	268	40	40	47	45
P	3.6	154	270	266	40	40	47	46
T		157	271	266	40	40	47	45
P	3.5	154	268	262	41	40	47	46
T		155	271	268	40	40	48	46
P	3.4	154	268	270	40	40	48	46
T		157	271	270	40	40	48	46
P	3.3	156	167	263	40	40	48	47
T		158	271	267	40	40	48	47
P	3.2	155	267	267	40	40	48	47
T		157	270	270	40	40	48	47
P	3.1	159	266	270	40	40	48	47
T		159	269	269	40	40	48	47
P	4.6	154	265	266	40	40	48	47
T		156	270	253	40	40	49	47
P	4.5	157	268	270	41	41	49	48
T		155	271	273	41	41	49	47
P	4.4	157	268	269	41	41	49	48
T		157	271	269	41	41	49	48
P	4.3	156	267	268	41	41	49	48
T		156	272	270	41	41	50	48
P	4.2	157	266	267	41	41	50	48
T		156	270	267	41	41	50	48
P	4.1	162	266	265	41	41	50	49
T		157	264	260	41	41	50	48
P TW Avg		156						
T TW Avg		158						

	Point No.	Pump Vac in Hg	Vel Head in H2O	Sqrt del P	Duct Vel fps	Sep P In in H2O	Opacity > 20%	Seconds > 20%
P	1.6		0.80	0.89	58.09		65	10
T		1	0.25	0.50	32.32			
P	1.5	2	0.50	0.71	45.55		20	1
T		1	0.20	0.45	28.88			
P	1.4	2	0.45	0.67	43.29			
T		1	0.20	0.45	28.90			
P	1.3	4	0.80	0.89	57.76		65	4
T		1	0.20	0.45	28.97			
P	1.2	4	1.00	1.00	64.53			
T		1	0.25	0.50	32.26			
P	1.1	6	1.70	1.30	84.34			
T		2	0.40	0.63	41.01			
P	2.6	5	1.30	1.14	73.51		20	0.9
T		1	0.35	0.59	38.27			
P	2.5	5	1.20	1.10	70.63			
T		1	0.30	0.55	35.40			
P	2.4	5.5	1.40	1.18	76.10			
T		1	0.40	0.63	40.94			
P	2.3	5	1.30	1.14	73.45		25	2
T		1	0.35	0.59	38.27			
P	2.2	6	1.40	1.18	76.35			
T		2	0.50	0.71	45.74			
P	2.1	6	1.70	1.30	84.13			
T		2	0.40	0.63	40.88			
P	3.6	6	1.60	1.26	81.49			
T		1	0.35	0.59	38.21			
P	3.5	6	1.60	1.26	81.49			
T		1	0.30	0.55	35.31			
P	3.4		0.95	0.97	62.79			
T		1	0.25	0.50	32.29			
P	3.3	3	0.80	0.89	57.72			
T		1	0.20	0.45	28.90			
P	3.2	4	0.95	0.97	62.84		30	1
T		1	0.25	0.50	32.29			
P	3.1		1.10	1.05	67.84			
T		1	0.25	0.50	32.34			
P	4.6	3	0.80	0.89	57.62			
T		1	0.25	0.50	32.26			
P	4.5	2	0.55	0.74	47.89			
T		1	0.15	0.39	24.97			
P	4.4	4	0.80	0.89	57.76			
T		1	0.25	0.50	32.29			
P	4.3	6	1.50	1.22	79.03			
T		1	0.30	0.55	35.34			
P	4.2	6	1.50	1.22	79.09			
T		1	0.30	0.55	35.34			
P	4.1	5	1.20	1.10	71.03			
T		1	0.25	0.50	32.29			
P TW Avg				1.04				
T TW Avg				0.53				

	Point No.	Separator P, in. WC	Annubar in. WC	Tank T deg F	Jet Flow gpm	Jet P psig	Jet Temp deg F	Gas T In deg F
P	1.6	11	2.9	429	355	295		140
T			1	429	115	287		133
P	1.5		2.9	429	355	295		133
T			1	429	115	287		126
P	1.4		2.9	429	355	295		140
T			1	429	115	287		153
P	1.3	10.5	2.95	429	355	295		154
T			1.05	429	115	287		140
P	1.2		2.95	429	355	295		147
T			1.05	429	115	287		126
P	1.1		2.95	429	350	295		147
T			1.05	429	115	287		133
P	2.6	10.5	3	429	350	295		147
T			0.95	429	115	287		133
P	2.5		3	429	350	292		140
T			0.95	429	115	285		126
P	2.4		3	429	350	292		133
T			0.95	429	115	285		119
P	2.3	10.5	3	429	350	292		147
T			1	429	115	285		126
P	2.2		3	429	350	292		140
T			1	429	115	285		126
P	2.1		3	429	350	292		147
T			1	429	115	285		133
P	3.6	10.5	3	429	350	295		147
T			0.95	429	115	287		133
P	3.5		3	429	350	295		140
T			0.95	429	115	287		133
P	3.4		3	429	350	295		147
T			0.95	429	115	287		126
P	3.3		3	429	350	295		140
T			0.95	429	115	287		126
P	3.2	10.5	3	429	350	295		147
T			1	429	115	287		133
P	3.1		3	429	350	295		154
T			1	429	115	287		133
P	4.6		3	429	350	295		147
T			1	429	115	287		133
P	4.5	10.5	2.95	429	350	295		140
T			1	429	115	287		133
P	4.4		2.95	429	350	295		154
T			1	429	115	287		133
P	4.3		2.95	429	350	295		154
T			1	429	115	287		140
P	4.2	10.5	2.95	429	350	295		147
T			1	429	115	287		133
P	4.1		2.95	429	350	295		147
T			1	429	115	287		133
P TW Avg			2.97	429	351	294	0	145
T TW Avg			0.99		115	287	0	132

LABORATORY DATA

Orsat Analysis

Operator

Run	1		2		3		Avg
Gas	Act %	Net %	Act %	Net %	Act %	Net %	Net %
CO2	2.0	2.0	2.0	2.0	2.0	2.0	2.0
O2	20.2	18.2	20.2	18.2	20.2	18.2	18.2
CO	20.4	0.2	20.4	0.2	20.4	0.2	0.2
N2		79.6		79.6		79.6	79.6
Molecular Weight, Dry			29.05				

Particulate Analysis

Front-half Filter Dry Catch, mg	8.99	
Blank Filter Catch, mg		None Used
Front-half Aqueous Wash, mg		
Filterable	9.07	
Non-filterable	13.69	
Front-half Acetone Wash, mg	3.02	
Impinger Catch, mg		
Filterable	1.40	
Non-filterable	Not Applicable	
Back-half Acetone rinse, mg	7.90	
Total Front-half Filterable, mg	18.06	
Total Front-half Nonfilterable, mg	16.71	

Total Front-half, mg	34.77	
Total Back-half Filterable, mg	1.40	

Total Pennsylvania DER Mass, mg	36.17	

CALCULATIONS

Standard Temp, deg F	68
Standard Press, in Hg	29.92
Barometric Press, in Hg	29.42
Stack Press, in Hg	29.41
Vol of H2O Std, dscf	14.573
M-5 Stack Moist. Content, %	30.38
Sat Stack Moist. Content, %	30.44
Stack Moist. Cont. Used, %	30.38
Molecular Weight, Dry	29.05
Molecular Weight, Wet	25.69
Nozzle Dia, in	0.296
X-Area of Stack, ft2	32.125

	Push	Travel	Total
Time-avg Stack Temp, deg F	156	158	157
Meter Volume Corr, ft3	22.292	11.162	33.454
Meter Volume Std, dscf	22.256	11.144	33.401
Vol of H2O Std, dscf	9.711	4.862	14.573
Sample Time, min	18.10	18.55	36.65
Stack Vel, fps	67.43	34.28	
Percent Isokinetic, %	109	105	
Stack Gas Vol, acfm	129968	66069	
Stack Gas Vol, dscfm	76222	38653	
Stack Gas Density, lb/ft3	0.0562	0.0561	
DER Part. Emission Conc., gr/dscf		0.0167	
DER Part. Emission Rate, lb/ton coke		0.0144	
DER Part. Emission Rate, lb/hr		0.76	
Front-half Part. Conc., gr/dscf		0.0161	
Front-half Part. Rate, lb/ton coke		0.0138	
Front-half Part. Rate, lb/hr		0.73	
Back-half Filt. Conc., gr/dscf		0.0006	
Back-half Filt. Rate, lb/ton coke		0.0006	
Back-half Filt. Rate, lb/hr		0.03	

**DUCT VELOCITIES
AT SAMPLING PLANE**

Push

Position	6	58	74	81	58
	5	46	71	81	48
	4	43	76	63	58
	3	58	73	58	79
	2	65	76	63	79
	1	84	84	68	71
		1	2	3	4
		Position			

Travel

Position	6	32	38	38	32
	5	29	35	35	25
	4	29	41	32	32
	3	29	38	29	35
	2	32	46	32	35
	1	41	41	32	32
		1	2	3	4
		Position			

FIELD DATA

Plant	USS - Clairton, PA
Date	12/06/84
Car No.	104
Battery No.	20
Sample Location	HCQC - Test Car
Sample Type	M-5
Run Number	7.2
Operator	Smith/Jarman
No. of Ovens Tested	24
No. of Ovens Tested/hr	4.8
Coke Prd'n Rate, tons/oven	14.5
Ambient Temp, deg F	30
Barometric Pressure, in Hg	29.01
Static Pressure, in H2O	-0.25
Stack Area, ft2	32.125
Filter Type	RA 934ah
Top Filter Number	RA102G-046
Bottom Filter Number	None
Probe Length & Type	5 ft - TFE Lined
Nozzle Size	0.301
Pitot Coefficient	0.84
Meter Box Number	APT 12 LG Mod
DGM Coeff's A1	0.0012
A2	1.0171
A3	0.0037
Orifice Coeff's B	0.4821
A	0.391
Cal Press, in Hg	29.65

	in Hg	CFM
Leak Check Initial	17	0.002
Final	16	0.002

Water Volume:

Location	Initial	Final	Net Gain
Imp A1	100	338	238
Imp A2	100	238	138
Imp A3	0	0	0
Sil Gel A	691.4	696.4	5
Imp B1	100	108	8
Imp B2	100	100	0
Imp B3	0	0	0
Sil Gel B	743.5	752.2	8.7
Total Volume			397.7

Combined Impinger pH	2.5
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	Point No.	Oven No.	Start Time	Sample Time		Gas Metr ft3	Rotometer	Orifice del P in. WC
				Total	sec DGM Start			
						321.875		
P	1.6	A-9	9:41	84	43	322.550	16	0.37
T					41	322.840		0.11
P	1.5	B-9	9:53	92	46	323.440	13.7	0.30
T					46	323.718		0.08
P	1.4	C-9	10:06	106	48	324.350	14.5	0.30
T					58	324.600		0.08
P	1.3	A-11	10:18	86	45	325.370	16.7	0.39
T					41	325.674		0.11
P	1.2	B-11	10:30	95	46	326.550	20.5	0.53
T					49	326.969	9.8	0.16
P	1.1	C-11	10:42	104	47	328.030	27	0.75
T					57	328.770	12.8	0.27
P	2.6	A-13	10:55	86	45	329.630	25.2	0.75
T					41	330.145	11.9	0.22
P	2.5	B-13	11:07	94	45	331.050	23	0.65
T					49	331.592	10.9	0.22
P	2.4	C-13	11:19	101	46	332.480	21.1	0.50
T					55	333.145	12.8	0.25
P	2.3	A-15	11:35	85	45	334.100	27	0.78
T					40	334.628	13.7	0.28
P	2.2	B-15	11:48	95	46	335.610	27	0.77
T					49	336.317	12.8	0.26
P	2.1	C-15	12:01	102	46	337.270	24.2	0.73
T					56	338.054	15.3	0.35
P	3.6	A-17	12:13	86	47	339.050		0.76
T					39	339.510		0.25
P	3.5	B-17	12:25	93	44	340.420	22.2	0.64
T					49	340.958	11.9	0.24
P	3.4	C-17	12:38	103	46	341.740	20.5	0.48
T					57	342.193	9.8	0.13
P	3.3	A-19	12:50	91	46	342.950	18.7	0.45
T					45	343.280	9.8	0.12
P	3.2	B-19	13:02	93	44	344.060	20.5	0.55
T					49	344.480	9.8	0.15
P	3.1	C-19	13:15	104	47	345.370	23.2	0.57
T					57	346.030	10.9	0.20
P	4.6	A-21	13:29	88	46	346.690	15.2	0.35
T					42	346.865		0.08
P	4.5	B-21	13:42	92	47	347.440	12.8	0.24
T					45	347.580		0.05
P	4.4	C-21	13:54	103	45	348.200	16.7	0.33
T					58	348.520		0.08
P	4.3	A-23	14:06	87	46	349.360	24.2	0.70
T					41	349.867	10.9	0.23
P	4.2	B-23	14:18	102	45	350.800	25.2	0.65
T					57	351.473	10.9	0.17
P	4.1	C-23	14:31	106	45	352.370	24.2	0.61
T					61	352.925	9.8	0.13
Total (Time in minutes)					37.97	31.05		
Push					18.27	19.797	File: DAT	702
Travel					19.70	11.253	Page 2 of 8	

Point		-----		Temperature, deg F			-----	
No.		Stack	Probe	Oven	Imping A	Imping B	GM In	GM Out
P	1.6	162	271	266	40	40	41	41
T		162	269	269	40	40	42	41
P	1.5	156	270	265	40	40	42	42
T		163	269	262	40	40	42	41
P	1.4	157	266	264	40	40	43	42
T		163	269	265	40	40	44	42
P	1.3	157	265	266	40	40	44	43
T		165	269	264	40	40	44	43
P	1.2	165	264	266	40	40	45	44
T		166	268	266	40	40	45	43
P	1.1	166	265	268	40	40	46	44
T		164	266	267	40	40	46	44
P	2.6	165	267	268	40	40	46	45
T		163	268	265	40	40	47	45
P	2.5	159	266	260	40	40	47	46
T		164	267	263	40	40	47	46
P	2.4	155	265	263	40	40	48	46
T		162	265	263	40	40	48	46
P	2.3	163	265	260	40	40	48	47
T		162	265	260	40	40	48	47
P	2.2	158	264	264	40	40	48	47
T		162	264	267	40	40	49	47
P	2.1	169	264	264	40	40	48	47
T		166	270	265	40	40	49	47
P	3.6	158	270	267	40	40	49	48
T		160	269	269	40	40	49	47
P	3.5	158	268	262	40	40	49	48
T		161	270	261	40	40	49	48
P	3.4	172	265	262	40	40	50	48
T		167	266	265	40	40	50	48
P	3.3	159	265	266	40	40	49	48
T		160	268	269	40	40	50	48
P	3.2	157	265	266	40	40	50	48
T		163	266	265	40	40	50	48
P	3.1	156	264	269	40	40	50	48
T		172	267	270	40	40	50	48
P	4.6	154	268	269	40	40	50	49
T		159	270	268	40	40	50	49
P	4.5	154	266	263	40	40	50	49
T		159	269	263	40	40	50	49
P	4.4	157	265	261	40	40	50	48
T		164	270	260	40	40	50	48
P	4.3	169	265	264	40	40	50	48
T		168	269	264	40	40	50	48
P	4.2	168	264	265	40	40	50	49
T		165	266	265	40	40	50	48
P	4.1	163	263	266	40	40	49	48
T		164	263	266	40	40	50	48
P TW Avg		161						
T TW Avg		164						

	Point No.	Pump Vac in Hg	Vel Head in H2O	Sqrt del P	Duct Vel fps	Sep P In in H2O	Opacity > 20%	Seconds > 20%
P	1.6	3	0.60	0.77	51.11			
T		1	0.20	0.45	29.51			
P	1.5	2	0.48	0.69	45.25		70	3
T		1	0.15	0.39	25.57			
P	1.4	3	0.50	0.71	46.47		65	5
T		1	0.15	0.39	25.57			
P	1.3	3	0.70	0.84	54.98			
T		1	0.20	0.45	29.58			
P	1.2	5	0.95	0.97	64.46		55	8
T		1	0.25	0.50	33.10			
P	1.1	7	1.90	1.38	91.24			
T		2	0.40	0.63	41.80			
P	2.6	7	1.40	1.18	78.26			
T			0.35	0.59	39.07			
P	2.5	5	1.20	1.10	72.10		30	1
T		1	0.30	0.55	36.20			
P	2.4	6	1.00	1.00	65.61		80	10
T		1	0.40	0.63	41.73			
P	2.3	7	1.60	1.26	83.52			
T			0.45	0.67	44.26			
P	2.2	7	1.60	1.26	83.19		90	9
T		2	0.40	0.63	41.73			
P	2.1	6.5	1.30	1.14	75.65		65	8
T		3	0.55	0.74	49.09			
P	3.6	7	1.60	1.26	83.19		40	3
T			0.35	0.59	38.97			
P	3.5	5	1.10	1.05	68.98		30	2
T		2	0.35	0.59	39.00			
P	3.4		0.95	0.97	64.82		80	10
T		1	0.25	0.50	33.12			
P	3.3	4	0.80	0.89	58.87		85	7
T		1	0.25	0.50	32.94			
P	3.2	5	0.95	0.97	64.05			
T		1	0.25	0.50	33.02			
P	3.1	7	1.20	1.10	71.93		100	21
T		2	0.30	0.55	36.43			
P	4.6	4	0.55	0.74	48.62		30	2
T		1	0.15	0.39	25.49			
P	4.5	3	0.40	0.63	41.46		35	2
T		1	0.10	0.32	20.81			
P	4.4	5	0.65	0.81	52.98		95	16
T		1	0.15	0.39	25.59			
P	4.3	9	1.30	1.14	75.65		100	27
T			0.30	0.55	36.31			
P	4.2	8	1.40	1.18	78.44		100	8
T		3	0.30	0.55	36.23			
P	4.1	8	1.30	1.14	75.29		30	1
T		2	0.25	0.50	33.04			
P TW Avg				1.01				
T TW Avg				0.52				

	Point No.	Separator P, in. WC	Annubar in. WC	Tank T deg F	Jet Flow gpm	Jet P psig	Jet Temp deg F	Gas T In deg F
P	1.6		3	429	350	292		147
T			1	429	115	285		133
P	1.5	10.5	3	429	350	295		154
T			1	429	115	287		140
P	1.4		3	429	350	295		147
T			1	429	115	287		140
P	1.3		3	429	350	297		147
T			1	429	115	290		133
P	1.2	10.5	3	429	350	297		147
T			1	429	115	290		133
P	1.1		3	429	350	295		147
T			1	429	115	290		133
P	2.6		3	429	350	295		147
T			1	429	115	290		133
P	2.5	10.5	3	429	350	295		154
T			0.95	429	115	287		126
P	2.4		3	429	350	295		147
T			0.95	429	115	287		133
P	2.3		3	429	350	295		147
T			0.95	429	115	287		126
P	2.2	10.5	3	429	350	295		140
T			0.95	429	115	287		126
P	2.1		3	429	350	295		140
T			0.95	429	115	287		126
P	3.6		3	429	350	295		140
T			0.95	429	115	287		126
P	3.5	10.5	3	429	350	295		147
T			0.95	429	115	287		126
P	3.4		3	429	350	295		140
T			0.95	429	115	287		133
P	3.3		3	429	350	295		140
T			0.95	429	115	287		126
P	3.2	10.5	3.05	429	350	295		147
T			0.95	429	115	287		126
P	3.1		3.05	429	350	295		147
T			0.95	429	115	285		133
P	4.6		3.05	429	350	290		133
T			0.95	429	115	282		119
P	4.5	10.5	3.05	429	350	295		140
T			0.95	429	115	285		140
P	4.4		3.05	429	350	295		154
T			0.95	429	115	287		140
P	4.3		3.05	429	350	295		147
T			0.95	429	115	287		133
P	4.2	10.5	3.05	429	350	295		140
T			0.95	429	115	287		133
P	4.1		3.05	429	350	295		147
T			0.95	429	115	287		126
P	TW Avg		3.02	429	350	295	0	145
T	TW Avg		0.96		115	287	0	131

LABORATORY DATA

Orsat Analysis

Operator

Run	1		2		3		Avg
Gas	Act %	Net %	Act %	Net %	Act %	Net %	Net %
CO2	2.2	2.2	2.2	2.2	2.2	2.2	2.2
O2	19.6	17.4	19.4	17.2	19.4	17.2	17.3
CO	19.8	0.2	19.8	0.4	19.8	0.4	0.3
N2		80.2		80.2		80.2	80.2
Molecular Weight, Dry			29.04				

Particulate Analysis

Front-half Filter Dry Catch, mg	43.67	
Blank Filter Catch, mg		None used
Front-half Aqueous Wash, mg		
Filterable	9.67	
Non-filterable	22.44	
Front-half Acetone Wash, mg	3.99	
Impinger Catch, mg		
Filterable	2.09	
Non-filterable		Not Applicable
Back-half Acetone rinse, mg	5.97	
Total Front-half Filterable, mg	53.34	
Total Front-half Nonfilterable, mg	26.43	

Total Front-half, mg	79.77	
Total Back-half Filterable, mg	2.09	

Total Pennsylvania DER Mass, mg	81.86	

CALCULATIONS

Standard Temp, deg F	68
Standard Press, in Hg	29.92
Barometric Press, in Hg	29.01
Stack Press, in Hg	28.99
Vol of H2O Std, dscf	18.720
M-5 Stack Moist. Content, %	37.47
Sat Stack Moist. Content, %	35.04
Stack Moist. Cont. Used, %	35.04
Molecular Weight, Dry	29.04
Molecular Weight, Wet	25.17
Nozzle Dia, in	0.301
X-Area of Stack, ft ²	32.125

	Push	Travel	Total
Time-avg Stack Temp, deg F	161	164	162
Meter Volume Corr, ft ³	20.237	11.493	31.730
Meter Volume Std, dscf	19.923	11.315	31.238
Vol of H2O Std, dscf	10.745	6.102	16.848
Sample Time, min	18.27	19.70	37.97
Stack Vel, fps	66.47	34.58	
Percent Isokinetic, %	103	105	
Stack Gas Vol, acfm	128130	66652	
Stack Gas Vol, dscfm	68609	35520	
Stack Gas Density, lb/ft ³	0.0539	0.0536	
DER Part. Emission Conc., gr/dscf		0.0404	
DER Part. Emission Rate, lb/ton coke		0.0324	
DER Part. Emission Rate, lb/hr		2.24	
Front-half Part. Conc., gr/dscf		0.0394	
Front-half Part. Rate, lb/ton coke		0.0316	
Front-half Part. Rate, lb/hr		2.18	
Back-half Filt. Conc., gr/dscf		0.0010	
Back-half Filt. Rate, lb/ton coke		0.0008	
Back-half Filt. Rate, lb/hr		0.06	

**DUCT VELOCITIES
AT SAMPLING PLANE**

Push

Position	6	51	78	83	49
	5	45	72	69	41
	4	46	66	65	53
	3	55	84	59	76
	2	64	83	64	78
	1	91	76	72	75
		1	2	3	4
		Position			

Travel

Position	6	30	39	39	25
	5	26	36	39	21
	4	26	42	33	26
	3	30	44	33	36
	2	33	42	33	36
	1	42	49	36	33
		1	2	3	4
		Position			

FIELD DATA

Plant	USS - Clairton, PA
Date	12/13/84
Car No.	104
Battery No.	20
Sample Location	HCQC - Test Car
Sample Type	M-5
Run Number	7.4
Operator	Jarman/Milburn
No. of Ovens Tested	24
No. of Ovens Tested/hr	4.7
Coke Prd'n Rate, tons/oven	14.5
Ambient Temp, deg F	60
Barometric Pressure, in Hg	29.24
Static Pressure, in H2O	-0.07
Stack Area, ft ²	32.125
Filter Type	RA 934ah
Top Filter Number	RA102G-048
Bottom Filter Number	None
Probe Length & Type	5 ft - TFE Lined
Nozzle Size	0.302
Pitot Coefficient	0.84
Meter Box Number	APT 12 LG Mod
DGM Coeff's A1	0.0012
A2	1.0171
A3	0.0037
Orifice Coeff's B	0.4821
A	0.391
Cal Press, in Hg	29.65

	in Hg	CFM
Leak Check Initial	16	0.006
Final	16	0.007

Water Volume:

Location	Initial	Final	Net Gain
Imp A1	100	398	298
Imp A2	100	101	1
Imp A3	0	1	1
Sil Gel A	673.4	678.6	5.2
Imp B1	100	138	38
Imp B2	100	102	2
Imp B3	0	1	1
Sil Gel B	662	671.8	9.8
Total Volume			356

Combined Impinger pH	3.0
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	Point No.	Oven No.	Start Time	Sample Time		Gas Metr ft3	Rotometer	Orifice del P in. WC
				Total	sec DGM Start			
						355.297		
P	1.6	B-1	9:30	89	45	356.070	21.1	0.50
T					44	356.675	12.8	0.23
P	1.5	C-1	9:42	103	47	357.290	16	
T					56	357.716		0.08
P	1.4	A-3	9:57	78	46	358.320	16.7	0.33
T					32	358.620		0.11
P	1.3	B-3	10:09	86	43	359.350	20.5	0.50
T					43	359.765	11.9	0.16
P	1.2	C-3	10:21	96	45	360.550	22.2	0.56
T					51	361.057	11.8	0.20
P	1.1	A-5	10:35	85	47	362.150	26	0.75
T					38	362.660	16.7	0.34
P	2.6	B-5	10:47	89	46	363.560	25.7	0.61
T					43	364.098	14.5	0.29
P	2.5	C-5	10:59	102	45	364.800	16.7	0.37
T					57	365.172		0.11
P	2.4	A-7	11:11	86	48	365.800	16	0.32
T					38	366.144	12.8	
P	2.3	B-7	11:24	86	44	367.090	28.6	0.77
T					42	367.739	16.7	0.36
P	2.2	C-7	11:36	100	45	368.730	26.2	0.78
T					55	369.482	15.3	0.37
P	2.1	A-9	11:49	83	46	370.470	25	0.75
T					37	371.065	17.4	
P	3.6	B-9	12:02	92	46	372.040	23.2	0.64
T					46	372.587	12.8	0.20
P	3.5	C-9	12:17	99	44	373.470	22.2	0.60
T					55	374.126	11.8	0.20
P	3.4	A-11	12:29	82	44	374.950	21.1	0.54
T					38	375.365	10.9	0.16
P	3.3	B-11	12:41	93	44	376.230	20	0.65
T					49	376.862	10.5	0.26
P	3.2	C-11	12:53	100	44	377.740	21.1	0.65
T					56	378.486	11.9	0.26
P	3.1	A-13	13:09	85	44	379.470	25.7	0.78
T					41	380.157	13.7	0.35
P	4.6	B-13	13:21	90	43	381.050	18	0.61
T					47	381.679	9.8	0.21
P	4.5	C-13	13:33	102	44	382.460	14.6	0.42
T					58	383.140		0.08
P	4.4	A-15	13:45	84	46	384.040	20.5	0.59
T					38	384.482	9.8	
P	4.3	B-15	13:58	98	45	385.500	26.2	0.78
T					53	386.383	13.7	0.40
P	4.2	C-15	14:10	102	46	387.450	26	0.77
T					56	388.301	12.8	0.35
P	4.1	A-17	14:23	85	45	389.300	26.2	0.79
T					40	389.450	11.9	0.32
Total (Time in minutes)					36.58	34.153		
Push					18.03	20.822	File: DAT	704
Travel					18.55	13.331	Page 2 of 8	

	Point No.	Temperature, deg F						GM In	GM Out
		Stack	Probe	Oven	Imping A	Imping B			
P	1.6		265	268	67	67	66	65	
T		160	270	269	65	65	66	64	
P	1.5	158	265	268	67	67	67	65	
T		161	268	268	62	62	68	66	
P	1.4	159	263	267	68	68	68	67	
T		161	266	269	66	66	69	67	
P	1.3	159	264	267	68	68	69	68	
T		161	268	264	64	63	68	68	
P	1.2	158	263	253	66	66	70	69	
T		162	266	250	61	61	71	69	
P	1.1	157	262	256	66	66	71	70	
T		155	264	258	58	58	72	70	
P	2.6	157	262	263	65	65	72	70	
T		159	267	258	60	58	72	70	
P	2.5	158	265	256	65	65	72	71	
T		160	266	256	60	60	72	70	
P	2.4	161	264	261	65	65	72	71	
T		160	264	259	60	60	72	70	
P	2.3	161	263	260	65	65	72	71	
T		162	262	260	59	59	72	72	
P	2.2	157	262	261	65	65	72	71	
T		163	265	262	59	59	72	71	
P	2.1	159	262	265	65	65	73	71	
T		160	261	265	59	58	73	71	
P	3.6	163	263	269	65	65	73	71	
T		163	267	268	69	59	73	71	
P	3.5	161	264	261	66	66	73	72	
T		160	267	262	60	60	73	72	
P	3.4	158	263	260	67	66	73	72	
T		157	269	262	60	60	73	71	
P	3.3	164	263	260	67	67	74	73	
T		161	267	259	60	60	74	72	
P	3.2	162	263	262	67	67	74	73	
T		162	264	263	60	60	74	73	
P	3.1	158	262	266	67	67	74	73	
T		160	266	268	60	60	75	73	
P	4.6	158	265	269	66	66	74	73	
T		160	269	269	59	59	74	73	
P	4.5	171	264	264	67	67	74	73	
T		163	265	263	61	61	75	73	
P	4.4	159	264	254	68	68	74	73	
T		159	267	258	60	60	75	73	
P	4.3	156	261	254	68	68	75	74	
T		160	264	257	60	60	75	74	
P	4.2	160	261	258	68	68	75	74	
T		161	263	259	60	60	75	74	
P	4.1	157	264	264	68	68	75	74	
T		160	260	263	60	60	75	74	
P TW Avg		160							
T TW Avg		161							

	Point No.	Pump Vac in Hg	Vel Head in H2O	Sqrt del P	Duct Vel fps	Sep P In in H2O	Opacity > 20%	Seconds > 20%
P	1.6		1.00	1.00	56.19			
T			0.40	0.63	41.26			
P	1.5		0.60	0.77	50.45			
T		1	0.15	0.39	25.29			
P	1.4	3	0.65	0.81	52.55			
T		1	0.20	0.45	29.20			
P	1.3	3	0.95	0.97	63.53			
T		1	0.35	0.59	38.62		25	1
P	1.2	3.5	1.00	1.00	65.13			
T		1	0.35	0.59	38.66			
P	1.1	6	2.00	1.41	92.03		25	1
T		2	0.65	0.81	52.38			
P	2.6	6	1.40	1.18	77.00			
T		2	0.50	0.71	46.09			
P	2.5	5	0.65	0.81	52.51			
T		2	0.20	0.45	29.17			
P	2.4	3	0.60	0.77	50.57			
T		2	0.40	0.63	41.26			
P	2.3	6	1.80	1.34	87.59			
T		3	0.65	0.81	52.68			
P	2.2	6	1.50	1.22	79.70			
T		2	0.55	0.74	48.50			
P	2.1	6	2.10	1.45	94.46			
T		2	0.70	0.84	54.58			
P	3.6	5	1.20	1.10	71.63			
T		1	0.40	0.63	41.36			
P	3.5	5	1.10	1.05	68.47			
T		1	0.35	0.59	38.59			
P	3.4	3.5	1.00	1.00	65.13			
T		1	0.30	0.55	35.64			
P	3.3		0.90	0.95	62.09			
T		1	0.27	0.52	33.92			
P	3.2	4	1.00	1.00	65.34			
T		2	0.35	0.59	38.66			
P	3.1	5	1.45	1.20	78.43		25	1
T		2	0.45	0.67	43.76			
P	4.6	4	0.75	0.87	56.40			
T		1	0.25	0.50	32.62			
P	4.5	3	0.50	0.71	46.54		45	5
T		1	0.15	0.39	25.33			
P	4.4	4	0.95	0.97	63.53			
T		1	0.25	0.50	32.59			
P	4.3	6	1.50	1.22	79.64			
T		2.5	0.45	0.67	43.76			
P	4.2	6	1.95	1.40	91.10			
T		2	0.40	0.63	41.29			
P	4.1	6	1.50	1.22	79.70			
T		1	0.35	0.59	38.59			
P TW Avg				1.06				
T TW Avg				0.60				

	Point No.	Separator P, in. WC	Annubar in. WC	Tank T deg F	Jet Flow gpm	Jet P psig	Jet Temp deg F	Gas T In deg F
P	1.6		3.1	414	365	295		203
T			1.5	414	115	287		175
P	1.5		3.1	414	365	295		210
T			1.5	414	115	287		182
P	1.4		3.1	414	365	295		189
T			1.5	414	115	287		175
P	1.3		3.1	414	365	295		189
T			1.5	414	115	285		175
P	1.2		3.1	414	360	295		196
T			1.5	414	115	285		168
P	1.1		3.1	414	360	295		203
T			1.5	414	115	285		175
P	2.6		3.1	414	360	295		203
T			1.5	414	115	285		168
P	2.5		3.05	414	365	295		203
T			1.5	414	115	285		175
P	2.4		3.05	414	365	295		196
T			1.5	414	115	287		168
P	2.3		3.05	414	365	295		189
T			1.45	414	115	287		168
P	2.2		3.05	414	365	295		210
T			1.45	414	115	287		189
P	2.1		3.05	414	365	295		196
T			1.45	414	115	287		168
P	3.6		3.05	414	370	295		203
T			1.45	414	115	287		175
P	3.5		3.05	414	365	295		203
T			1.45	414	115	287		175
P	3.4		3.05	414	365	295		196
T			1.45	414	115	287		168
P	3.3		3.05	414	365	295		203
T			1.45	414	115	285		175
P	3.2		3.05	414	365	295		203
T			1.5	414	115	287		175
P	3.1		3.05	414	365	295		203
T			1.5	414	115	287		175
P	4.6		3.05	414	365	295		203
T			1.5	414	115	287		175
P	4.5		3.05	414	365	295		203
T			1.5	414	115	287		175
P	4.4		3.05	414	365	295		196
T			1.5	414	115	287		175
P	4.3		3.05	414	365	295		196
T			1.5	414	115	287		175
P	4.2		3.05	414	365	295		196
T			1.5	414	115	287		175
P	4.1		3.05	414	365	295		203
T			1.5	414	115	287		175
P	TW Avg		3.06	414	365	295	0	200
T	TW Avg		1.49		115	286	0	174

LABORATORY DATA

Orsat Analysis

Operator

Run	1		2		3		Avg
Gas	Act %	Net %	Act %	Net %	Act %	Net %	Net %
CO2	1.8	1.8	2.2	2.2	2.2	2.2	2.1
O2	20.2	18.4	20.4	18.2	20.4	18.2	18.3
CO	20.2	0.0	20.4	0.0	20.4	0.0	0.0
N2		79.8		79.6		79.6	79.7
Molecular Weight, Dry			29.06				

Particulate Analysis

Front-half Filter Dry Catch, mg	8.27
Blank Filter Catch, mg	None Used
Front-half Aqueous Wash, mg	
Filterable	5.57
Non-filterable	26.07
Front-half Acetone Wash, mg	5.82
Impinger Catch, mg	
Filterable	1.69
Non-filterable	Not Applicable
Back-half Acetone rinse, mg	6.63
Total Front-half Filterable, mg	13.84
Total Front-half Nonfilterable, mg	31.89

Total Front-half, mg	45.73
Total Back-half Filterable, mg	1.69

Total Pennsylvania DER Mass, mg	47.42

CALCULATIONS

Standard Temp, deg F	68
Standard Press, in Hg	29.92
Barometric Press, in Hg	29.24
Stack Press, in Hg	29.23
Vol of H2O Std, dscf	16.757
M-5 Stack Moist. Content, %	32.60
Sat Stack Moist. Content, %	33.02
Stack Moist. Cont. Used, %	32.60
Molecular Weight, Dry	29.06
Molecular Weight, Wet	25.45
Nozzle Dia, in	0.302
X-Area of Stack, ft ²	32.125

	Push	Travel	Total
Time-avg Stack Temp, deg F	160	161	160
Meter Volume Corr, ft ³	21.289	13.617	34.905
Meter Volume Std, dscf	21.125	13.512	34.637
Vol of H2O Std, dscf	10.220	6.537	16.757
Sample Time, min	18.03	18.55	36.58
Stack Vel, fps	69.16	38.92	
Percent Isokinetic, %	101	112	
Stack Gas Vol, acfm	133306	75021	
Stack Gas Vol, dscfm	74808	42034	
Stack Gas Density, lb/ft ³	0.0551	0.0550	
DER Part. Emission Conc., gr/dscf		0.0211	
DER Part. Emission Rate, lb/ton coke		0.0185	
DER Part. Emission Rate, lb/hr		1.26	
Front-half Part. Conc., gr/dscf		0.0204	
Front-half Part. Rate, lb/ton coke		0.0178	
Front-half Part. Rate, lb/hr		1.22	
Back-half Filt. Conc., gr/dscf		0.0008	
Back-half Filt. Rate, lb/ton coke		0.0007	
Back-half Filt. Rate, lb/hr		0.04	

**DUCT VELOCITIES
AT SAMPLING PLANE**

Push

Position	6	56	77	72	56
	5	50	53	68	47
	4	53	51	65	64
	3	64	88	62	80
	2	65	80	65	91
	1	92	94	78	80
		1	2	3	4
		Position			

Travel

Position	6	41	46	41	33
	5	25	29	39	25
	4	29	41	36	33
	3	39	53	34	44
	2	39	48	39	41
	1	52	55	44	39
		1	2	3	4
		Position			

FIELD DATA

Plant	USS - Clairton, PA
Date	12/14/84
Car No.	104
Battery No.	20
Sample Location	HCQC - Test Car
Sample Type	M-5
Run Number	7.5
Operator	Jarman/Milburn
No. of Ovens Tested	24
No. of Ovens Tested/hr	4.4
Coke Prd'n Rate, tons/oven	14.5
Ambient Temp, deg F	60
Barometric Pressure, in Hg	29.5
Static Pressure, in H ₂ O	-0.1
Stack Area, ft ²	32.125
Filter Type	RA 934ah
Top Filter Number	RA102G-049
Bottom Filter Number	None
Probe Length & Type	5 ft - TFE Lined
Nozzle Size	0.301
Pitot Coefficient	0.84
Meter Box Number	APT 12 LG Mod
DGM Coeff's A1	0.0012
A2	1.0171
A3	0.0037
Orifice Coeff's B	0.4821
A	0.391
Cal Press, in Hg	29.65

	in Hg	CFM
Leak Check Initial	18	0.001
Final	19	0.001

Water Volume:

Location	Initial	Final	Net Gain
Imp A1	100	412	312
Imp A2	100	114	14
Imp A3	0	0	0
Sil Gel A	641	646.5	5.5
Imp B1	100	120	20
Imp B2	100	100	0
Imp B3	0	0	0
Sil Gel B	654	664	10
Total Volume			361.5

Combined Impinger pH	3.5
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	Point No.	Oven No.	Start Time	Sample Time		Gas Metr ft3	Rotometer	Orifice del P in. WC
				Total	DGM Start			
						393.111		
P	1.6	C-15	8:56	106	45	393.970	20.5	0.57
T					61	394.674	11.9	0.25
P	1.5	A-17	9:09	88	44	395.360	16	0.42
T					44	395.564		0.11
P	1.4	B-17	9:23	99	46	396.370	17.4	0.54
T					53	396.800		0.08
P	1.3	C-17	9:36	104	45	397.640	20	0.55
T					59	398.216	9.8	0.17
P	1.2	A-19	9:48	88	44	399.020	23.2	0.70
T					44	399.610	12.8	0.29
P	1.1	B-19	10:01	94	46	400.610	27	0.82
T					48	401.403	15.3	0.34
P	2.6	C-19	10:13	103	46	402.360	23.7	0.69
T					57	403.112	12.8	0.29
P	2.5	A-21	10:26	84	46	404.050	22.2	0.69
T					38	404.495	12.8	0.22
P	2.4	B-21	10:38	99	46	405.420	23.7	0.73
T					53	406.158	14.5	0.36
P	2.3	C-21	10:51	101	45	406.900	16	0.38
T					56	407.410		0.08
P	2.2	B-23	11:17	97	44	408.370	27	0.81
T					53	409.079	12.8	0.24
P	2.1	C-23	11:29	100	43	409.960	20	0.51
T					57	410.657	11.9	0.21
P	3.6	A-25	11:41	90	45	411.550	25.2	0.79
T					45	412.047	12.8	0.22
P	3.5	B-25	11:56	99	43	412.900	24.2	0.74
T					56	413.625	13.7	0.26
P	3.4	C-25	12:10	104	44	414.430	20.5	0.53
T					60	415.043	10.9	0.20
P	3.3	A-27	12:23	94	44	415.800	18.7	0.51
T					50	416.300	9.8	0.17
P	3.2	B-27	12:36	100	44	417.050	20.5	0.55
T					56	417.653	10.9	0.22
P	3.1	C-27	12:48	102	43	418.490	24.2	0.73
T					59	419.232	12.6	0.24
P	4.6	A-29	13:01	91	45	419.990	18	0.49
T					46	420.369	9.8	0.15
P	4.5	B-29	13:14	100	44	420.970	12.8	0.27
T					56	421.325		0.08
P	4.4	A-2	13:40	84	44	422.060	20.5	0.52
T					40	422.238	10.9	
P	4.3	B-2	13:58	92	43	422.980	23.2	0.79
T					49	423.280	10.9	0.16
P	4.2	C-2	14:11	98	44	424.110	25.7	0.76
T					54	424.470	11.9	0.18
P	4.1	A-4	14:24	87	44	425.310	25.2	
T					43	425.610	13.7	0.25
Total (Time in minutes)				38.40	32.499			
Push				17.78	19.799	File: DAT		
Travel				20.62	12.700	Page 2 of 8		
						705		

	Point No.	Temperature, deg F						
		Stack	Probe	Oven	Imping A	Imping B	GM In	GM Out
P	1.6	157	259	267	54	55	53	52
T		160	263	268	50	50	54	52
P	1.5	163	261	260	55	55	54	54
T		163	265	261	51	51	55	53
P	1.4	157	260	261	55	55	56	54
T		162	263	261	50	50	56	54
P	1.3	157	261	263	55	55	56	55
T		162	263	259	50	50	57	55
P	1.2	159	260	259	55	54	57	56
T		162	263	259	50	50	58	56
P	1.1	160	260	259	57	57	58	57
T		161	261	264	50	50	59	57
P	2.6	173	264	263	56	56	59	58
T		167	265	260	50	50	60	58
P	2.5	157	262	259	56	56	59	59
T		158	261	259	50	50	60	60
P	2.4	159	262	256	57	56	60	59
T		159	261	257	50	50	60	59
P	2.3	159	261	260	57	57	61	60
T		160	260	259	50	50	61	60
P	2.2	160	260	259	57	57	62	60
T		157	260	262	51	51	62	60
P	2.1	160	259	267	58	58	63	61
T		160	259	258	50	50	63	61
P	3.6	155	264	268	58	58	63	62
T		152	265	267	50	50	64	62
P	3.5	163	263	259	58	58	64	62
T		157	265	262	50	50	64	62
P	3.4	156	262	259	59	59	64	63
T		155	264	260	50	50	64	63
P	3.3	157	261	259	59	59	65	64
T		162	264	259	51	51	65	64
P	3.2	152	261	256	60	60	65	64
T		158	262	257	52	52	66	64
P	3.1	157	260	262	60	60	65	66
T		158	261	263	52	52	66	65
P	4.6	152	264	266	61	61	66	65
T		156	266	268	54	54	67	66
P	4.5	150	262	258	61	61	67	66
T		155	263	261	54	54	67	66
P	4.4	158	262	259	62	62	68	67
T		157	266	260	54	54	68	67
P	4.3	154	261	257	62	62	68	67
T		154	265	262	60	60	68	67
P	4.2	159	260	264	62	62	69	68
T		159	261	264	60	60	69	68
P	4.1	160	262	263	62	62	69	68
T		159	263	264	60	60	69	68
P TW Avg		158						
T TW Avg		159						

	Point No.	Pump Vac in Hg	Vel Head in H2O	Sqrt del P	Duct Vel fps	Sep P In in H2O	Opacity > 20%	Seconds > 20%
P	1.6		0.90	0.95	61.33			
T		1	0.35	0.59	38.34			
P	1.5		0.60	0.77	50.31			
T		1	0.20	0.45	29.05			
P	1.4		0.70	0.84	54.08			
T		1	0.15	0.39	25.14			
P	1.3		0.90	0.95	61.33			
T		1	0.25	0.50	32.45			
P	1.2		1.20	1.10	70.93			
T		1	0.40	0.63	41.05			
P	1.1		2.10	1.45	93.90			
T		2	0.55	0.74	48.10			
P	2.6		1.25	1.12	73.20		65	1
T		2	0.40	0.63	41.21			
P	2.5		1.10	1.05	67.80			
T		2	0.40	0.63	40.92			
P	2.4		1.25	1.12	72.39			
T		3	0.50	0.71	45.78			
P	2.3		0.60	0.77	50.15			
T		1	0.15	0.39	25.10			
P	2.2	6.5	1.60	1.26	81.97			
T		2	0.40	0.63	40.88			
P	2.1		0.90	0.95	61.47			
T		3	0.35	0.59	38.34			
P	3.6		1.40	1.18	76.36			
T		1	0.40	0.63	40.72			
P	3.5		1.30	1.14	74.06			
T		2	0.45	0.67	43.36			
P	3.4		0.95	0.97	62.95		60	3
T		1	0.30	0.55	35.35			
P	3.3		0.80	0.89	57.82			
T		1	0.25	0.50	32.45			
P	3.2		0.95	0.97	62.75			
T		1	0.13	0.36	23.33			
P	3.1		1.30	1.14	73.70			
T		2	0.39	0.62	40.40			
P	4.6		0.75	0.87	55.75			
T		1	0.25	0.50	32.30			
P	4.5		0.40	0.63	40.65			
T		1	0.15	0.39	25.00			
P	4.4		0.95	0.97	63.06			
T		1	0.30	0.55	35.41			
P	4.3		1.10	1.05	67.63			
T		2	0.30	0.55	35.32			
P	4.2		1.45	1.20	77.97			
T		1	0.35	0.59	38.31			
P	4.1		1.40	1.18	76.67			
T		2	0.45	0.67	43.43			

P TW Avg
T TW Avg

1.02
0.56

	Point No.	Separator P, in. WC	Annubar in. WC	Tank T deg F	Jet Flow gpm	Jet P psig	Jet Temp deg F	Gas T In deg F
P	1.6		3.1	414	360	295		203
T			1.35	414	120	285		175
P	1.5	11	3.1	414	365	295		210
T			1.35	414	120	285		182
P	1.4		3.1	414	360	295		203
T			1.35	414	120	287		175
P	1.3		3.1	414	365	295		203
T			1.35	414	120	287		175
P	1.2	11	3.05	414	365	295		203
T			1.35	414	120	287		175
P	1.1		3.05	414	365	295		203
T			1.35	414	115	287		175
P	2.6		3.05	414	360	295		203
T			1.35	414	115	287		182
P	2.5	11	3.05	414	360	295		203
T			1.35	414	120	287		175
P	2.4		3.05	414	360	295		203
T			1.35	414	120	287		175
P	2.3		3.05	414	360	295		203
T			1.35	414	120	287		175
P	2.2		3.05	414	365	295		196
T			1.35	414	120	287		175
P	2.1		3.05	414	365	295		203
T			1.35	414	120	287		175
P	3.6	11	3.05	414	365	295		189
T			1.35	414	120	287		175
P	3.5		3.05	414	360	295		189
T			1.35	414	120	287		161
P	3.4		3.05	414	360	295		175
T			1.35	414	115	287		161
P	3.3	11	3.05	414	360	295		203
T			1.35	414	120	287		175
P	3.2		3.05	414	360	295		196
T			1.4	414	120	287		168
P	3.1		3.05	414	360	295		196
T			1.4	414	120	287		168
P	4.6	11	3.05	414	360	295		203
T			1.4	414	120	287		175
P	4.5		3.05	414	360	295		203
T			1.35	414	120	287		175
P	4.4		3.05	414	355	295		196
T			1.35	414	120	287		168
P	4.3		3.05	414	345	295		154
T			1.35	414	115	287		140
P	4.2	11	3.05	414	360	275		196
T			1.35	414	120	270		161
P	4.1		3.05	414	360	295		182
T			1.35	414	120	287		161
P	TW Avg		3.06	414	361	294	0	197
T	TW Avg		1.36		119	286	0	171

LABORATORY DATA

Orsat Analysis

Operator

Run	1		2		3		Avg
Gas	Act %	Net %	Act %	Net %	Act %	Net %	Net %
CO2	1.8	1.8	2.2	2.2	2.2	2.2	2.1
O2	20.2	18.4	20.4	18.2	20.4	18.2	18.3
CO	20.2	0.0	20.4	0.0	20.4	0.0	0.0
N2		79.8		79.6		79.6	79.7
Molecular Weight, Dry			29.06				

Particulate Analysis

Front-half Filter Dry Catch, mg	9.98
Blank Filter Catch, mg	None used
Front-half Aqueous Wash, mg	
Filterable	2.35
Non-filterable	15.58
Front-half Acetone Wash, mg	2.17
Impinger Catch, mg	
Filterable	1.46
Non-filterable	Not Applicable
Back-half Acetone rinse, mg	3.55
Total Front-half Filterable, mg	12.33
Total Front-half Nonfilterable, mg	17.75

Total Front-half, mg	30.08
Total Back-half Filterable, mg	1.46

Total Pennsylvania DER Mass, mg	31.54

**DUCT VELOCITIES
AT SAMPLING PLANE**

Push

Position	6	61	73	76	56
	5	50	68	74	41
	4	54	72	63	63
	3	61	50	58	68
	2	71	82	63	78
	1	94	61	74	77
		1	2	3	4
		Position			

Travel

Position	6	38	41	41	32
	5	29	41	43	25
	4	25	46	35	35
	3	32	25	32	35
	2	41	41	23	38
	1	48	38	40	43
		1	2	3	4
		Position			

FIELD DATA

Plant	USS - Clairton, PA
Date	10/19/84
Car No.	104
Battery No.	20
Sample Location	HCQC - Test Car
Sample Type	M-5
Run Number	3.1
Operator	Jarman/Smith
No. of Ovens Tested	24
No. of Ovens Tested/hr	4.2
Coke Prd'n Rate, tons/oven	14.5
Ambient Temp, deg F	78
Barometric Pressure, in Hg	30.45
Static Pressure, in H2O	0.5
Stack Area, ft2	32.125
Filter Type	RA 934 AH
Top Filter Number	RA102G-017
Bottom Filter Number	RA102G-022
Probe Length & Type	5 ft - TFE Lined
Nozzle Size	0.302
Pitot Coefficient	0.84
Meter Box Number	APT 12 LG Mod
DGM Coeff's A1	0.0012
A2	1.0171
A3	0.0037
Orifice Coeff's B	0.4821
A	0.391
Cal Press, in Hg	29.65

	in Hg	CFM
Leak Check Initial	16	0.000
Final	15	0.001

Water Volume:

Location	Initial	Final	Net Gain
Imp A1	100	284	184
Imp A2	100	300	200
Imp A3	0	0	0
Sil Gel A	658.7	666.5	7.8
Imp B1	100	236	136
Imp B2	100	102.2	2.2
Imp B3	0	0	0
Sil Gel B	659.2	666.9	7.7
Total Volume			537.7

Combined Impinger pH	3.5
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	Point No.	Oven No.	Start Time	Sample Time		Gas Metr ft3	Rotometer	Orifice del P in. WC
				Total	DGM Start			
						752.570		
P	1.6	C-21		111	49	753.360		0.43
T					62	753.929		0.11
P	1.5	A-23		95	52	754.610		0.30
T					43	754.879		0.08
P	1.4	B-23		100	51	755.580		0.32
T					49	755.923		0.08
P	1.3	A-25		92	49	756.740		
T					43	757.171		
P	1.2	B-25		104	52	758.050		
T					52	758.719		0.25
P	1.1	C-25		106	50	759.900		1.10
T					56	760.810		
P	2.6	A-27		84	49	761.850		0.86
T					35	762.403		0.39
P	2.5	B-27		101	50	763.410		0.73
T					51	764.108		0.27
P	2.4	C-27		111	50	765.100		0.71
T					61	765.996		0.34
P	2.3	A-29		98	49	767.080		0.88
T					49	767.848		0.38
P	2.2	B-29		104	50	769.000		0.95
T					54	769.840		0.39
P	2.1	C-29		110	50	771.100		1.10
T					60	772.095		0.40
P	3.6	A-2		81	47	773.160		0.97
T					34	773.640		0.35
P	3.5	B-2		92	48	774.690		0.91
T					44	775.363		0.37
P	3.4	C-2		96	48	776.330		0.75
T					48	776.945		0.26
P	3.3	A-4		82	48	777.820		0.57
T					34	778.253		0.23
P	3.2	B-4		90	48	779.120		0.60
T					42	779.609		0.21
P	3.1	C-4		103	50	780.680		0.87
T					53	781.475		0.30
P	4.6	A-6		81	44	782.430		0.85
T					37	782.935		0.28
P	4.5	B-6		92	44	783.540		
T					48	783.928		0.08
P	4.4	C-6		100	49	784.800		0.67
T					51	785.490		0.24
P	4.3	A-8		80	47	786.530		
T					33	787.046		0.33
P	4.2	B-8		91	49	788.150		0.97
T					42	788.725		0.30
P	4.1	A-10		86	49	789.701		0.83
T					37	790.151		
Total (Time in minutes)					38.17	37.581		
Push					19.53	23.031	File: DAT	301
Travel					18.63	14.550	Page 2 of 8	

Point No.		----- Stack Probe		Temperature, deg F ----- Oven Imping A Imping B		GM In	GM Out
P	1.6	157	276	244	79	72	72
T		163	275	248	67	72	71
P	1.5	155	274	243	79	75	73
T		159	273	256	65	75	73
P	1.4	153	274	249	80	77	75
T		157	276	258	67	78	76
P	1.3	155	273	246	80	79	77
T		158	276	253	67	81	80
P	1.2	156	273	252	81	83	82
T		159	274	252	63	85	82
P	1.1	150	272	254	83	86	84
T		157	272	257	60	87	84
P	2.6	157	274	258	83	87	85
T		156	272	261	61	88	85
P	2.5	150	274	256	83	88	86
T		158	274	254	63	88	86
P	2.4	153	274	254	83	89	87
T		160	270	287	62	89	87
P	2.3	162	273	253	82	90	88
T		159	270	252	61.5	91	88
P	2.2	157	273	252	83	91	90
T		159	272	252	61.5	91	89
P	2.1	156	273	253	83	91	90
T		159	269	252	61.5	92	89
P	3.6	151	274	252	83	91	90
T		157	274	260	61	92	90
P	3.5	151	274	252	83	92	90
T		154	274	256	63	92	90
P	3.4	150	273	234	83	92	91
T		154	274	259	64	92	90
P	3.3	153	273	255	83	92	91
T		157	273	253	65	92	90
P	3.2	152	273	254	83	93	91
T		157	274	253	63	92	90
P	3.1	154	273	254	83	92	92
T		157	272	259	61	92	90
P	4.6	153	273	253	83	92	91
T		156	270	254	63	95	95
P	4.5	155	274	254	81	92	91
T		154	271	256	61	93	91
P	4.4	154	273	254	81	93	92
T		155	273	253	61	93	91
P	4.3	153	272	255	78	92	91
T		158	272	257	60	92	90
P	4.2	156	272	253	77	92	90
T		158	273	258	59	91	90
P	4.1	157	269	248	79	90	89
T		159	268	251	59	89	98
P TW Avg		154					
T TW Avg		158					

	Point No.	Pump Vac in Hg	Vel Head in H2O	Sqrt del P	Duct Vel fps	Sep P In in H2O	Opacity > 20%	Seconds > 20%
P	1.6	3	0.83	0.91	57.86			
T		1	0.20	0.45	28.54			
P	1.5	2	0.45	0.67	42.54			
T		1	0.15	0.39	24.64			
P	1.4		0.53	0.72	45.87			
T			0.15	0.39	24.60			
P	1.3		0.95	0.97	61.80			
T		1	0.25	0.50	31.78			
P	1.2	5	1.15	1.07	68.05			
T		2	0.35	0.59	37.63			
P	1.1		2.20	1.48	93.67			
T		2	0.65	0.81	51.20			
P	2.6		1.70	1.30	82.81			
T			0.60	0.77	49.16			
P	2.5	5	1.40	1.18	74.72			
T		3	0.45	0.67	42.64			
P	2.4	5	1.40	1.18	74.90			
T		3	0.55	0.74	47.22			
P	2.3	7	1.70	1.30	83.14			
T		3	0.60	0.77	49.28			
P	2.2	7	1.80	1.34	85.21			
T		3	0.60	0.77	49.28			
P	2.1	9.5	2.40	1.55	98.31			
T			0.75	0.87	55.09			
P	3.6	7	1.90	1.38	87.12			
T		2.5	0.55	0.74	47.10			
P	3.5	7	1.70	1.30	82.41			
T		2.5	0.55	0.74	46.99			
P	3.4	5	1.40	1.18	74.72			
T		2	0.40	0.63	40.07			
P	3.3	4.5	1.00	1.00	63.31			
T		2	0.33	0.57	36.48			
P	3.2	4.5	1.20	1.10	69.29			
T			0.31	0.56	35.36			
P	3.1	6.5	1.80	1.34	85.00			
T		2.5	0.50	0.71	44.91			
P	4.6	6	1.60	1.26	80.08			
T			0.50	0.71	44.87			
P	4.5		0.60	0.77	49.12			
T			0.15	0.39	24.54			
P	4.4	5	1.30	1.14	72.24			
T		2	0.40	0.63	40.10			
P	4.3	7	1.90	1.38	87.26			
T		2	0.50	0.71	44.95			
P	4.2	7	2.00	1.41	89.75			
T		3	0.50	0.71	44.95			
P	4.1	7	1.70	1.30	82.81			
T			0.75	0.87	55.09			
P	TW Avg			1.18				
T	TW Avg			0.65				

	Point No.	Separator P, in. WC	Annubar in. WC	Tank T deg F	Jet Flow gpm	Jet P psig	Jet Temp deg F	Gas T In deg F
P	1.6		4	420	400	290	420	154
T			1.6	420	110	275	420	147
P	1.5		4	420	400	290	420	154
T			1.6	420	110	280	420	168
P	1.4		4	426	400	295	420	147
T			1.6	426	110	285	420	168
P	1.3		4	432	408	290	430	140
T			1.6	432	110	280	430	168
P	1.2		4	432	408	295	420	154
T			1.6	432	110	285	420	252
P	1.1		4.4	432	408	310	426	147
T			1.6	432	110	295	426	168
P	2.6		2.6	432	400	305	426	133
T			1.2	432	110	290	426	147
P	2.5		2.6	432	400	300	420	140
T			1.2	432	110	290	420	196
P	2.4		2.5	432	400	300	426	140
T			1.2	432	110	290	420	154
P	2.3		2.5	432	400	300	420	140
T			1.2	432	110	290	414	168
P	2.2		2.5	432	400	300	420	140
T			1.2	432	110	290	414	154
P	2.1		2.5	432	400	300	420	154
T			1.2	432	110	290	420	168
P	3.6		2.5	432	400	300	420	140
T			1.2	432	110	290	414	210
P	3.5		2.5	432	400	300	420	140
T			1.2	432	110	290	414	154
P	3.4		2.5	432	400	300	414	140
T			1.2	432	110	290	414	168
P	3.3			426	400	300	414	126
T				426	110	290	414	154
P	3.2			426	400	300	414	140
T				426	110	290	414	154
P	3.1			426	400	300	414	147
T				426	110	290	414	168
P	4.6			426	400	300	414	140
T				426	110	290	414	154
P	4.5			426	400	300	414	140
T				426	110	290	414	154
P	4.4			426	400	300	414	133
T				426	110	290	414	154
P	4.3			426	400	300	408	140
T				426	110	290	408	140
P	4.2			426	400	300	420	133
T				426	110	290	420	140
P	4.1			426	400	300	420	140
T				426	110	290	420	154
P	TW Avg		2.00	429	401	299	419	142
T	TW Avg		0.90		110	288	418	166

LABORATORY DATA

Orsat Analysis

Operator - DaRos

Run	1		2		3		Avg
Gas	Act %	Net %	Act %	Net %	Act %	Net %	Net %
CO2	1.8	1.8	1.8	1.8	1.8	1.8	1.8
O2	19.6	17.8	21.0	19.2	20.4	18.6	18.5
CO	19.6	0.0	21.0	0.0	20.4	0.0	0.0
N2		80.4		79.0		79.6	79.7
Molecular Weight, Dry			29.03				

Particulate Analysis

Front-half Filter Dry Catch, mg	11.81
Blank Filter Catch, mg	-0.33
Front-half Aqueous Wash, mg	
Filterable	5.19
Non-filterable	17.15
Front-half Acetone Wash, mg	3.15
Impinger Catch, mg	
Filterable	1.08
Non-filterable	Not Applicable
Back-half Acetone rinse, mg	7.18
Total Front-half Filterable, mg	16.67
Total Front-half Nonfilterable, mg	20.30

Total Front-half, mg	36.97
Total Back-half Filterable, mg	1.08

Total Pennsylvania DER Mass, mg	38.05

CALCULATIONS

Standard Temp, deg F	68
Standard Press, in Hg	29.92
Barometric Press, in Hg	30.45
Stack Press, in Hg	30.49
Vol of H2O Std, dscf	25.310
M-5 Stack Moist. Content, %	38.94
Sat Stack Moist. Content, %	28.61
Stack Moist. Cont. Used, %	28.61
Molecular Weight, Dry	29.03
Molecular Weight, Wet	25.87
Nozzle Dia, in	0.302
X-Area of Stack, ft2	32.125

	Push	Travel	Total
Time-avg Stack Temp, deg F	154	158	156
Meter Volume Corr, ft3	23.549	14.863	38.412
Meter Volume Std, dscf	24.335	15.359	39.694
Vol of H2O Std, dscf	9.753	6.156	15.909
Sample Time, min	19.53	18.63	38.17
Stack Vel, fps	74.62	41.48	
Percent Isokinetic, %	90	107	
Stack Gas Vol, acfm	143837	79949	
Stack Gas Vol, dscfm	89946	49714	
Stack Gas Density, lb/ft3	0.0589	0.0585	
DER Part. Emission Conc., gr/dscf		0.0148	
DER Part. Emission Rate, lb/ton coke		0.0163	
DER Part. Emission Rate, lb/hr		1.00	
Front-half Part. Conc., gr/dscf		0.0144	
Front-half Part. Rate, lb/ton coke		0.0158	
Front-half Part. Rate, lb/hr		0.97	
Back-half Filt. Conc., gr/dscf		0.0004	
Back-half Filt. Rate, lb/ton coke		0.0005	
Back-half Filt. Rate, lb/hr		0.03	

**DUCT VELOCITIES
AT SAMPLING PLANE**

Push

Position	6	58	83	87	80
	5	43	75	82	49
	4	46	75	75	72
	3	62	83	63	87
	2	68	85	69	90
	1	94	98	85	83
		1	2	3	4
		Position			

Travel

Position	6	29	49	47	45
	5	25	43	47	25
	4	25	47	40	40
	3	32	49	36	45
	2	38	49	35	45
	1	51	55	45	55
		1	2	3	4
		Position			

FIELD DATA

Plant	USS - Clairton, PA
Date	10-21-84
Car No.	104
Battery No.	20
Sample Location	HCQC - Test Car
Sample Type	M-5
Run Number	3.2
Operator	Jarman/Smith
No. of Ovens Tested	12
No. of Ovens Tested/hr	4.0
Coke Prd'n Rate, tons/oven	14.5
Ambient Temp, deg F	~50
Barometric Pressure, in Hg	30.41
Static Pressure, in H2O	-0.5
Stack Area, ft ²	32.125
Filter Type	RA 934 AH
Top Filter Number	RA102G-021
Bottom Filter Number	RA102G-020
Probe Length & Type	5 ft - TFE Lined
Nozzle Size	0.302
Pitot Coefficient	0.84
Meter Box Number	APT 12 LG Mod
DGM Coeff's A1	0.0012
A2	1.0171
A3	0.0037
Orifice Coeff's B	0.4821
A	0.391
Cal Press, in Hg	29.65

	in Hg	CFM
Leak Check Initial	15	0.006
Final	15	0.010

Water Volume:

Location	Initial	Final	Net Gain
Imp A1	100	284	184
Imp A2	100	96	-4
Imp A3	0	0	0
Sil Gel A	666.9	671.8	4.9
Imp B1	100	138	38
Imp B2	100	101	1
Imp B3	0	0	0
Sil Gel B	666.5	671.4	4.9
Total Volume			228.8

Combined Impinger pH	3.5
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[illegible]

LABORATORY DATA

Orsat Analysis

Operator - DaRos

Run	1		2		3		Avg
Gas	Act %	Net %	Act %	Net %	Act %	Net %	Net %
CO2	2.8	2.8	2.7	2.7	2.7	2.7	2.7
O2	20.0	17.3	20.0	17.3	20.0	17.3	17.3
CO	20.2	0.2	20.2	0.2	20.1	0.1	0.2
N2		79.8		79.8		79.9	79.8
Molecular Weight, Dry			29.13				

Particulate Analysis

Front-half Filter Dry Catch, mg	7.76
Blank Filter Catch, mg	-0.23
Front-half Aqueous Wash, mg	
Filterable	1.31
Non-filterable	3.66
Front-half Acetone Wash, mg	2.80
Impinger Catch, mg	
Filterable	1.41
Non-filterable	Not Applicable
Back-half Acetone rinse, mg	5.85
Total Front-half Filterable, mg	8.84
Total Front-half Nonfilterable, mg	6.46

Total Front-half, mg	15.30
Total Back-half Filterable, mg	1.41

Total Pennsylvania DER Mass, mg	16.71

CALCULATIONS

Standard Temp, deg F	68
Standard Press, in Hg	29.92
Barometric Press, in Hg	30.41
Stack Press, in Hg	30.37
Vol of H2O Std, dscf	10.770
M-5 Stack Moist. Content, %	35.79
Sat Stack Moist. Content, %	29.97
Stack Moist. Cont. Used, %	29.97
Molecular Weight, Dry	29.13
Molecular Weight, Wet	25.79
Nozzle Dia, in	0.302
X-Area of Stack, ft2	32.125

	Push	Travel	Total
Time-avg Stack Temp, deg F	156	159	158
Meter Volume Corr, ft3	12.328	6.393	18.721
Meter Volume Std, dscf	12.723	6.597	19.320
Vol of H2O Std, dscf	5.445	2.823	8.268
Sample Time, min	10.42	9.22	19.63
Stack Vel, fps	68.87	40.20	
Percent Isokinetic, %	98	99	
Stack Gas Vol, acfm	132752	77491	
Stack Gas Vol, dscfm	80884	46960	
Stack Gas Density, lb/ft3	0.0583	0.0580	
DER Part. Emission Conc., gr/dscf		0.0133	
DER Part. Emission Rate, lb/ton coke		0.0140	
DER Part. Emission Rate, lb/hr		0.81	
Front-half Part. Conc., gr/dscf		0.0122	
Front-half Part. Rate, lb/ton coke		0.0128	
Front-half Part. Rate, lb/hr		0.74	
Back-half Filt. Conc., gr/dscf		0.0011	
Back-half Filt. Rate, lb/ton coke		0.0012	
Back-half Filt. Rate, lb/hr		0.07	

**DUCT VELOCITIES
AT SAMPLING PLANE**

Push

Position	6	51	70	0	0
	5	40	57	0	0
	4	45	75	0	0
	3	55	83	0	0
	2	71	86	0	0
	1	92	99	0	0
		1	2	3	4

Position

Travel

Position	6	29	45	0	0
	5	25	41	0	0
	4	25	47	0	0
	3	33	47	0	0
	2	40	49	0	0
	1	49	59	0	0
		1	2	3	4

Position

FIELD DATA

Plant	USS - Clairton, PA
Date	10-23-84
Car No.	104
Battery No.	20
Sample Location	HCQC - Test Car
Sample Type	M-5
Run Number	3.3
Operator	Jarman/Smith
No. of Ovens Tested	24
No. of Ovens Tested/hr	3.4
Coke Prd'n Rate, tons/oven	14.5
Ambient Temp, deg F	50
Barometric Pressure, in Hg	30.8
Static Pressure, in H2O	-0.5
Stack Area, ft ²	32.125
Filter Type	RA 934 AH
Top Filter Number	RA102G-025
Bottom Filter Number	RA102G-026
Probe Length & Type	5 ft - TFE Lined
Nozzle Size	0.302
Pitot Coefficient	0.84
Meter Box Number	APT 12 LG Mod
DGM Coeff's A1	0.0012
A2	1.0171
A3	0.0037
Orifice Coeff's B	0.4821
A	0.391
Cal Press, in Hg	29.65

	in Hg	CFM
Leak Check Initial	16	0.006
Final	10	0.005

Water Volume:

Location	Initial	Final	Net Gain
Imp A1	100	399	299
Imp A2	100	100	0
Imp A3	0	0	0
Sil Gel A	670.6	676.4	5.8
Imp B1	100	152	52
Imp B2	100	101	1
Imp B3	0	0	0
Sil Gel B	658.5	667.3	8.8
Total Volume			366.6

Combined Impinger pH	3.0
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	Point No.	Oven No.	Start Time	Sample Time		Gas Metr ft3	Rotometer	Orifice del P in. WC
				Total	sec DGM Start			
						834.663		
P	1.6	A-17		85	50	835.430		0.38
T					35	835.711		0.11
P	1.5	B-17		95	48	836.350		0.31
T					47	836.720		0.05
P	1.4	C-17		106	49	837.440		0.36
T					57	837.896		0.11
P	1.3	A-19		93	47	838.690		0.42
T					46	839.112		
P	1.2	B-19		98	46	839.970		0.65
T					52	840.610		0.19
P	1.1	C-19		103	48	841.700		0.92
T					55	842.448		0.31
P	2.6	A-21		87	49	843.400		0.56
T					38	843.863		0.23
P	2.5	B-21		98	48	844.800		0.62
T					50	845.415		0.23
P	2.4	C-21		100	47	846.300		0.62
T					53	846.995		0.26
P	2.3	A-23		88	46	847.970		0.78
T					42	848.535		0.24
P	2.2	B-23		96	47	849.540		0.80
T					49	850.176		0.20
P	2.1	C-23		105	48	851.370		1.10
T					57	852.258		0.35
P	3.6	A-25		87	48	853.290		0.74
T					39	853.837		0.29
P	3.5	B-25		97	48	854.900		0.81
T					49	855.522		0.24
P	3.4	C-25		105	49	856.330		0.48
T					56	856.871		0.11
P	3.3	A-29		93	49	857.700		0.52
T					44	858.228		0.22
P	3.2	B-29		94	47	859.030		0.48
T					47	859.485		0.15
P	3.1	C-29		107	46	860.470		0.78
T					61	861.221		0.23
P	4.6	A-2		84	47	862.120		0.53
T					37	862.482		0.16
P	4.5	B-2		92	45	863.150		0.30
T					47	863.355		
P	4.4	C-2		97	48	864.240		0.56
T					49	864.829		0.23
P	4.3	A-4		80	47	865.840		0.80
T					33	866.253		0.22
P	4.2	B-4		92	50	867.370		0.84
T					42	867.903		0.21
P	4.1	C-4		101	47	868.880		0.73
T					54	869.595		0.25

Total (Time in minutes)
Push
Travel

38.05
19.07
18.98

34.932
21.892
13.040

File: DAT
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	Point No.	Stack	Probe	Temperature, deg F				
				Oven	Imping A	Imping B	GM In	GM Out
P	1.6	153	271					
T		160	274					
P	1.5	157	270					
T		162	273					
P	1.4	159	271					
T		165	272					
P	1.3	154	270					
T		163	274					
P	1.2	152	270					
T		160	271					
P	1.1	160	270					
T		164	272					
P	2.6	155	270					
T		163	272					
P	2.5	152	271					
T		157	272					
P	2.4	151	270					
T		157	272					
P	2.3	151	271					
T		157	274					
P	2.2	159	271					
T		160	272					
P	2.1	159	269					
T		159	272					
P	3.6	153	271					
T		157	273					
P	3.5	155	270					
T		158	272					
P	3.4	159	269					
T		158	272					
P	3.3	152	272					
T		159	273					
P	3.2	154	273					
T		158	273					
P	3.1	154	272					
T		158	273					
P	4.6	157	273					
T		155	274					
P	4.5	154	272					
T		157	272					
P	4.4	153	271					
T		156	272					
P	4.3	155	271					
T		157	271					
P	4.2	154	270					
T		158	271					
P	4.1	154	270					
T		157	269					
P	TW Avg	155						
T	TW Avg	159						

	Point No.	Pump Vac in Hg	Vel Head in H2O	Sqrt del P	Duct Vel fps	Sep P In in H2O	Opacity > 20%	Seconds > 20%
P	1.6	3	0.65	0.81	50.85			
T		1	0.20	0.45	28.37			
P	1.5		0.55	0.74	46.93			
T		0	0.10	0.32	20.09			
P	1.4	3	0.55	0.74	47.01			
T		0	0.15	0.39	24.67			
P	1.3	3.5	0.75	0.87	54.67			
T			0.25	0.50	31.79			
P	1.2	4.5	1.20	1.10	69.04			
T		1	0.35	0.59	37.53			
P	1.1	7	1.80	1.34	85.11			
T		2.5	0.52	0.72	45.89			
P	2.6	4	0.90	0.95	59.94			
T			0.35	0.59	37.62			
P	2.5	4.5	1.10	1.05	66.10			
T		1	0.35	0.59	37.44			
P	2.4	4	1.10	1.05	66.05			
T		2	0.35	0.59	37.44			
P	2.3	5	1.40	1.18	74.51			
T		2	0.45	0.67	42.45			
P	2.2	6	1.50	1.22	77.63			
T			0.45	0.67	42.55			
P	2.1	7	2.30	1.52	96.13			
T		3	0.55	0.74	47.01			
P	3.6		1.30	1.14	71.92			
T		2	0.38	0.62	39.01			
P	3.5		1.50	1.22	77.38			
T		2	0.35	0.59	37.47			
P	3.4	4	1.00	1.00	63.38			
T		0	0.20	0.45	28.32			
P	3.3	3.5	0.90	0.95	59.79			
T			0.28	0.53	33.54			
P	3.2	3.5	0.85	0.92	58.20			
T		1	0.26	0.51	32.29			
P	3.1	5	1.30	1.14	71.98			
T		2	0.35	0.59	37.47			
P	4.6		0.96	0.98	62.00			
T		1	0.27	0.52	32.83			
P	4.5	3	0.50	0.71	44.64			
T		0	0.15	0.39	24.51			
P	4.4	4	1.00	1.00	63.08			
T		2	0.29	0.54	34.05			
P	4.3	6	1.40	1.18	74.75			
T		2	0.35	0.59	37.44			
P	4.2	7	1.60	1.26	79.85			
T			0.35	0.59	37.47			
P	4.1	6	1.30	1.14	71.98			
T		2	0.35	0.59	37.44			
P TW Avg				1.05				
T TW Avg				0.56				

	Point No.	Separator P, in. WC	Annubar in. WC	Tank T deg F	Jet Flow gpm	Jet P psig	Jet Temp deg F	Gas T In deg F
P	1.6			432	408	305	408	147
T				432	110	295	414	140
P	1.5			432	408	305	426	140
T				432	110	295	426	140
P	1.4			432	400	310	408	140
T				432	110	300	408	140
P	1.3			432	396	295	414	126
T				432	110	285	414	133
P	1.2			432	396	310	414	140
T				432	110	300	414	140
P	1.1			432	396	305	426	147
T				432	110	295	426	147
P	2.6			432	396	305	414	147
T				432	110	295	414	147
P	2.5			432	375	300	420	133
T				432	110	290	420	133
P	2.4			429	375	285	426	126
T				429	110	275	426	133
P	2.3			429	360	285	426	133
T				429	110	275	423	133
P	2.2			429	375	295	423	140
T				429	110	285	423	147
P	2.1			429	375	295	420	154
T				429	110	285	420	140
P	3.6			429	375	295	420	154
T				429	110	285	420	147
P	3.5			429	375	295	426	147
T				429	110	285	426	147
P	3.4			429	375	295	420	161
T				429	110	285	420	147
P	3.3			429	375	295	420	168
T				429	110	285	420	147
P	3.2			429	375	295	420	161
T				429	110	285	420	140
P	3.1			429	375	295	420	154
T				429	110	285	420	140
P	4.6			429	375	295	410	168
T				429	110	285	410	147
P	4.5			429	375	295	410	154
T				429	110	285	410	147
P	4.4			429	375	295	402	154
T				429	110	285	402	140
P	4.3			429	375	295	410	154
T				429	110	285	410	147
P	4.2			429	375	295	410	147
T				429	110	285	410	140
P	4.1			429	375	295	410	154
T				429	110	285	410	140
P TW Avg			0.00	430	382	297	417	148
T TW Avg			0.00		110	287	417	142

LABORATORY DATA

Orsat Analysis

Operator - DaRos

Run	1		2		3		Avg
Gas	Act %	Net %	Act %	Net %	Act %	Net %	Net %
CO2	2.0	2.0	2.0	2.0	2.0	2.0	2.0
O2	20.0	18.0	20.0	18.0	20.0	18.0	18.0
CO	20.2	0.2	20.2	0.2	20.2	0.2	0.2
N2		79.8		79.8		79.8	79.8
Molecular Weight, Dry			29.04				

Particulate Analysis

Front-half Filter Dry Catch, mg	4.97
Blank Filter Catch, mg	0.10
Front-half Aqueous Wash, mg	
Filterable	3.70
Non-filterable	12.94
Front-half Acetone Wash, mg	5.16
Impinger Catch, mg	
Filterable	1.35
Non-filterable	Not Applicable
Back-half Acetone rinse, mg	7.55
Total Front-half Filterable, mg	8.77
Total Front-half Nonfilterable, mg	18.10

Total Front-half, mg	26.87
Total Back-half Filterable, mg	1.35

Total Pennsylvania DER Mass, mg	28.22

CALCULATIONS

Standard Temp, deg F	68
Standard Press, in Hg	29.92
Barometric Press, in Hg	30.80
Stack Press, in Hg	30.76
Vol of H2O Std, dscf	17.256
M-5 Stack Moist. Content, %	31.62
Sat Stack Moist. Content, %	29.09
Stack Moist. Cont. Used, %	29.09
Molecular Weight, Dry	29.04
Molecular Weight, Wet	25.83
Nozzle Dia, in	0.302
X-Area of Stack, ft2	32.125

	Push	Travel	Total
Time-avg Stack Temp, deg F	155	159	157
Meter Volume Corr, ft3	22.382	13.319	35.701
Meter Volume Std, dscf	23.395	13.922	37.317
Vol of H2O Std, dscf	9.599	5.712	15.311
Sample Time, min	19.07	18.98	38.05
Stack Vel, fps	66.36	35.30	
Percent Isokinetic, %	99	112	
Stack Gas Vol, acfm	127908	68038	
Stack Gas Vol, dscfm	80079	42308	
Stack Gas Density, lb/ft3	0.0592	0.0588	
DER Part. Emission Conc., gr/dscf		0.0117	
DER Part. Emission Rate, lb/ton coke		0.0112	
DER Part. Emission Rate, lb/hr		0.54	
Front-half Part. Conc., gr/dscf		0.0111	
Front-half Part. Rate, lb/ton coke		0.0106	
Front-half Part. Rate, lb/hr		0.52	
Back-half Filt. Conc., gr/dscf		0.0006	
Back-half Filt. Rate, lb/ton coke		0.0005	
Back-half Filt. Rate, lb/hr		0.03	

DUCT VELOCITIES
AT SAMPLING PLANE

Push

Position	6	51	60	72	62
	5	47	66	77	45
	4	47	66	63	63
	3	55	75	60	75
	2	69	78	58	80
	1	85	96	72	72
		1	2	3	4
		Position			

Travel

Position	6	28	38	39	33
	5	20	37	37	25
	4	25	37	28	34
	3	32	42	34	37
	2	38	43	32	37
	1	46	47	37	37
		1	2	3	4
		Position			

FIELD DATA

Plant	USS - Clairton, PA
Date	10-24-84
Car No.	104
Battery No.	20
Sample Location	HCQC - Test Car
Sample Type	M-5
Run Number	3.4
Operator	Jarman/Smith
No. of Ovens Tested	24
No. of Ovens Tested/hr	4.5
Coke Prd'n Rate, tons/oven	14.5
Ambient Temp, deg F	~60
Barometric Pressure, in Hg	30.79
Static Pressure, in H2O	-0.5
Stack Area, ft ²	32.125
Filter Type	RA 934 AH
Top Filter Number	RA102G-030
Bottom Filter Number	RA102G-031
Probe Length & Type	5 ft - TFE Lined
Nozzle Size	0.302
Pitot Coefficient	0.84
Meter Box Number	APT 12 LG Mod
DGM Coeff's A1	0.0012
A2	1.0171
A3	0.0037
Orifice Coeff's B	0.4821
A	0.391
Cal Press, in Hg	29.65

	in Hg	CFM
Leak Check Initial	17	0.006
Final	15	0.000

Water Volume:

Location	Initial	Final	Net Gain
Imp A1	100	381	281
Imp A2	100	102	2
Imp A3	0	0	0
Sil Gel A	676.4	682	5.6
Imp B1	100	78	-22
Imp B2	100	101	1
Imp B3	0	0	0
Sil Gel B	663.3	672.2	8.9
Total Volume			276.5

Combined Impinger pH	3.0
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	Point No.	-----		Temperature, deg F -----			
		Stack	Probe	Oven	Imping A	Imping B	GM In GM Out
P	1.6	154	271	241	59		
T		162	272	247	50		
P	1.5	157	269	250	59		
T		161	272	249	55		
P	1.4	157	271	245	59		
T		161	273	249	54.5		
P	1.3	156	270	252	60		
T		170	271	254	50		
P	1.2	157	269	254	60		
T		161	271	251	55		
P	1.1	154	270		60		
T		161	269	252	53		
P	2.6	155	272	261	62		
T		162	276	260	53		
P	2.5	155	270	256	62		
T		163	271	258	56		
P	2.4	157	270	260	63		
T		163	270	258	57		
P	2.3	157	268	253	64		
T		160	269	250	57		
P	2.2	155	269	254	64		
T		160	269	253	57		
P	2.1	158	269	257	64		
T		162	268	254	57		
P	3.6	153	268	255	64		
T		160	268	255	58		
P	3.5	155	271	255	64		
T		158	270	256	58.5		
P	3.4	156	270	264	63		
T		160	270	267	58		
P	3.3	157	271	270	64		
T		158	271	265	59		
P	3.2	154	270	260	64		
T		160	270	258	59		
P	3.1	157	268	252	64		
T		160	270	247	57.5		
P	4.6	154	269	252	64		
T		156	272	254	57		
P	4.5	156	270	260	64		
T		159	272	262	59		
P	4.4	155	270	260	64		
T		160	272	260	57		
P	4.3	153	270	261	64		
T		159	272	260	58.5		
P	4.2	154	268	255	64		
T		160	271	253	59		
P	4.1	154	268	249	64		
T		159	268	249	57		

P TW Avg		155					
T TW Avg		161					

	Point No.	Pump Vac in Hg	Vel Head in H2O	Sqrt del P	Duct Vel fps	Sep P In in H2O	Opacity > 20%	Seconds > 20%
P	1.6	3	0.65	0.81	50.96			
T			0.25	0.50	31.81			
P	1.5	2	0.52	0.72	45.69			
T			0.15	0.39	24.62			
P	1.4	2	0.50	0.71	44.80			
T		1	0.20	0.45	28.43			
P	1.3	4	0.75	0.87	54.83			
T		1	0.25	0.50	32.01			
P	1.2	4.5	1.00	1.00	63.36			
T			0.30	0.55	34.81			
P	1.1	7	0.20	0.45	28.27			
T			0.50	0.71	44.95			
P	2.6	5	1.20	1.10	69.29			
T		2	0.35	0.59	37.63			
P	2.5	5	1.10	1.05	66.34			
T			0.40	0.63	40.27			
P	2.4	6	1.30	1.14	72.24			
T			0.50	0.71	45.02			
P	2.3		1.50	1.22	77.60			
T		2	0.45	0.67	42.60			
P	2.2	6	1.50	1.22	77.47			
T		2	0.45	0.67	42.60			
P	2.1	8	2.00	1.41	89.67			
T		3.5	0.70	0.84	53.22			
P	3.6	5	1.20	1.10	69.18			
T			0.40	0.63	40.17			
P	3.5	6.5	1.60	1.26	80.01			
T		2	0.45	0.67	42.54			
P	3.4	4	0.95	0.97	61.70			
T			0.25	0.50	31.76			
P	3.3	4	0.90	0.95	60.11			
T		1	0.30	0.55	34.73			
P	3.2	4	0.85	0.92	58.27			
T			0.30	0.55	34.79			
P	3.1	5	1.10	1.05	66.45			
T			0.40	0.63	40.17			
P	4.6	3	0.65	0.81	50.96			
T		1	0.25	0.50	31.65			
P	4.5	3	0.60	0.77	49.04			
T			0.15	0.39	24.58			
P	4.4	4.5	1.00	1.00	63.26			
T		2	0.30	0.55	34.79			
P	4.3	6	1.30	1.14	72.00			
T		2	0.35	0.59	37.54			
P	4.2	7	1.60	1.26	79.95			
T			0.40	0.63	40.17			
P	4.1	6	1.30	1.14	72.06			
T			0.32	0.57	35.90			
P TW Avg				1.00				
T TW Avg				0.58				

	Point No.	Separator P, in. WC	Annubar in. WC	Tank T deg F	Jet Flow gpm	Jet P psig	Jet Temp deg F	Gas T In deg F
P	1.6		2.6	426	375	287	408	147
T			1.25	426	110	280	408	154
P	1.5		2.6	429	375	290	414	147
T			1.25	429	110	280	414	140
P	1.4		2.6	429	375	295	417	147
T			1.25	429	110	285	417	140
P	1.3		2.7	429	375	297	420	161
T			1.25	429	110	287	420	154
P	1.2		2.7	429	375	295	423	161
T			1.2	429	110	285	423	147
P	1.1		2.7	429	375	295	426	161
T			1.2	429	110	285	426	147
P	2.6		2.6	426	375	300	426	161
T			1.2	426	110	295	420	140
P	2.5		2.6	429	375	295	429	182
T			1.4	429	110	285	429	161
P	2.4		2.6	429	375	295	420	175
T			1.4	429	110	285	420	154
P	2.3		2.7	429	375	295	426	161
T			1.4	429	110	285	426	147
P	2.2		2.7	429	375	297	429	168
T			1.3	429	110	285	429	154
P	2.1		2.7	429	375	297	426	182
T			1.3	429	110	287	426	147
P	3.6		2.65	429	375	300	429	182
T			1.3	429	110	290	429	147
P	3.5		2.65	429	375	297	426	168
T			1.3	429	110	290	426	154
P	3.4		2.65	429	375	297	429	154
T			1.3	429	110	287	429	147
P	3.3		2.65	429	375	292	426	175
T			1.3	429	110	285	426	140
P	3.2		2.6	429	375	295	429	154
T			1.3	429	110	290	429	147
P	3.1		2.6	429	375	295	429	175
T			1.3	429	110	287	429	147
P	4.6		2.6	429	360	292	426	161
T			1.3	429	110	282	426	147
P	4.5		2.6	429	370	297	426	161
T			1.3	429	110	287	426	154
P	4.4		2.7	429	370	297	426	175
T			1.3	429	110	287	426	140
P	4.3		2.7	429	370	297	426	168
T			1.25	429	110	287	426	147
P	4.2		2.7	429	370	297	426	168
T			1.25	429	110	287	426	140
P	4.1		2.7	429	370	297	426	168
T			1.25	429	110	287	426	140
P	TW Avg		2.65	429	373	295	424	165
T	TW Avg		1.28		110	286	424	147

LABORATORY DATA

Orsat Analysis

Operator - DaRos

Run	1		2		3		Avg
Gas	Act %	Net %	Act %	Net %	Act %	Net %	Net %
CO2	2.2	2.2	2.2	2.2	2.2	2.2	2.2
O2	20.6	18.4	20.4	18.2	20.6	18.4	18.3
CO	20.9	0.3	20.6	0.2	20.9	0.3	0.3
N2		79.1		79.4		79.1	79.2
Molecular Weight, Dry			29.09				

Particulate Analysis

Front-half Filter Dry Catch, mg	14.00
Blank Filter Catch, mg	-0.05
Front-half Aqueous Wash, mg	
Filterable	4.00
Non-filterable	19.56
Front-half Acetone Wash, mg	0.47
Impinger Catch, mg	
Filterable	2.31
Non-filterable	Not Applicable
Back-half Acetone rinse, mg	5.24
Total Front-half Filterable, mg	17.95
Total Front-half Nonfilterable, mg	20.03

Total Front-half, mg	37.98
Total Back-half Filterable, mg	2.31

Total Pennsylvania DER Mass, mg	40.29

CALCULATIONS

Standard Temp, deg F	68
Standard Press, in Hg	29.92
Barometric Press, in Hg	30.79
Stack Press, in Hg	30.75
Vol of H2O Std, dscf	13.015
M-5 Stack Moist. Content, %	34.43
Sat Stack Moist. Content, %	29.87
Stack Moist. Cont. Used, %	29.87
Molecular Weight, Dry	29.09
Molecular Weight, Wet	25.77
Nozzle Dia, in	0.302
X-Area of Stack, ft2	32.125

	Push	Travel	Total
Time-avg Stack Temp, deg F	155	161	158
Meter Volume Corr, ft3	23.696	0.022	23.718
Meter Volume Std, dscf	24.760	0.023	24.783
Vol of H2O Std, dscf	10.546	0.010	10.556
Sample Time, min	18.92	18.05	36.97
Stack Vel, fps	63.38	36.78	
Percent Isokinetic, %	112	0	
Stack Gas Vol, acfm	122166	70893	
Stack Gas Vol, dscfm	75550	43467	
Stack Gas Density, lb/ft3	0.0590	0.0585	
DER Part. Emission Conc., gr/dscf		0.0251	
DER Part. Emission Rate, lb/ton coke		0.0228	
DER Part. Emission Rate, lb/hr		1.48	
Front-half Part. Conc., gr/dscf		0.0236	
Front-half Part. Rate, lb/ton coke		0.0215	
Front-half Part. Rate, lb/hr		1.39	
Back-half Filt. Conc., gr/dscf		0.0014	
Back-half Filt. Rate, lb/ton coke		0.0013	
Back-half Filt. Rate, lb/hr		0.08	

DUCT VELOCITIES
AT SAMPLING PLANE

Push

Position	6	51	69	69	51
	5	46	66	80	49
	4	45	72	62	63
	3	55	78	60	72
	2	63	77	58	80
	1	28	90	66	72
		1	2	3	4

Position

Travel

Position	6	32	38	40	32
	5	25	40	43	25
	4	28	45	32	35
	3	32	43	35	38
	2	35	43	35	40
	1	45	53	40	36
		1	2	3	4

Position