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BENZENE SAMPLING PROGRAM  
AT COKE BY-PRODUCT RECOVERY PLANTS:  
REPUBLIC STEEL CORPORATION  
GADSDEN, ALABAMA

EPA Contract 68-02-2813  
Work Assignment 48  
ESED Project No. 74/4j

Prepared For:

Mr. Daniel Bivins  
U. S. Environmental Protection Agency  
Office of Air Quality Planning and Standards  
Emission Measurement Branch, ESED, MD-13  
Research Triangle Park, North Carolina 27711

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SCOTT ENVIRONMENTAL SERVICES  
A Division Of  
SCOTT ENVIRONMENTAL TECHNOLOGY, INC.  
Plumsteadville, Pennsylvania 18949



Scott Environmental Technology Inc.

TABLE OF CONTENTS

Page No.

1.0 INTRODUCTION	1-1
2.0 SUMMARY OF RESULTS	2-1
3.0 RESULTS AND DISCUSSION	3-1
4.0 PROCESS DESCRIPTION	4-1
5.0 FIELD SAMPLING AND ANALYSIS METHODOLOGY	5-1
5.1 TRACER TESTING	5-1
5.2 SAMPLE HANDLING	5-1
5.3 FIELD ANALYSIS	5-2
6.0 FIELD SAMPLING PROCEDURES	6-1
6.1 LIGHT OIL INTERCEPTING SUMP	6-1
7.0 LABORATORY SAMPLE ANALYSIS	7-1
7.1 SAMPLE PREPARATION	7-1
7.2 PURGE AND TRAP PROCEDURE FOR EXTRACTION OF BENZENE FROM LIQUID PHASE TO GASEOUS PHASE	7-2
7.3 GAS CHROMATOGRAPH	7-4
8.0 QUALITY CONTROL AND QUALITY ASSURANCE	8-1
8.1 FIELD ANALYSIS PROCEDURES	8-1
8.2 PROCEDURES FOR ANALYSIS OF PROCESS LIQUIDS	8-2

APPENDICES

- APPENDIX A - SAMPLE CALCULATIONS
- APPENDIX B - FIELD DATA SHEETS
- APPENDIX C - LABORATORY DATA SHEETS
- APPENDIX D - TRACER GAS METHOD DEVELOPMENT
- APPENDIX E - PROJECT PARTICIPANTS



## 1.0 INTRODUCTION

Scott Environmental Services, a division of Scott Environmental Technology, Inc. conducted a testing program at Republic Steel Corporation in Gadsden, Alabama to determine benzene emissions from one source in the coke by-product recovery plant. The work was performed for the United States Environmental Protection Agency, Emissions Measurement Branch, under Contract No. 68-02-2813, Work Assignment 48. Republic Steel was one of seven plants visited to collect data for a possible National Emission Standard for Hazardous Air Pollutants for benzene.

Sampling was conducted at Republic Steel on October 16 and 17, 1980. Air and liquid samples for benzene analysis were collected from the light oil intercepting sump.



## 2.0 SUMMARY OF RESULTS

## LIGHT OIL INTERCEPTING SUMP - TRACER DATA SUMMARY

		<u>Benzene Emission Rate</u>	
		<u>lb/hr</u>	<u>kg/hr</u>
Test 1	Run 1	4.27	1.94
	Run 2	4.50	2.05
Test 2	Run 1	5.41	2.46
	Run 2	5.21	2.37
Test 3	Run 1	6.29	2.86
	Run 2	5.13	2.33
Avg.		5.14	2.38

## LIQUID SAMPLE DATA

<u>Sample Location</u>	<u>Date</u>	<u>Time</u>	<u>Sample Temp. (°F)</u>	<u>Benzene Concentration (ppm by weight)</u>
West Side - Inlet	10/16/80	11:25	87	25,800
Middle	10/16/80	11:27	82	27,900
Outlet	10/16/80	11:30	114	18.0
East Side - Inlet	10/16/80	11:35	146	97.1
Middle	10/16/80	11:37	139	86.7
Outlet	10/16/80	11:40	156	1.0



### 3.0 RESULTS AND DISCUSSION

The light oil intercepting sump is comprised of two separate halves, called east and west for identification purposes. Figure 3-1 shows the sump configuration and location of samplers.

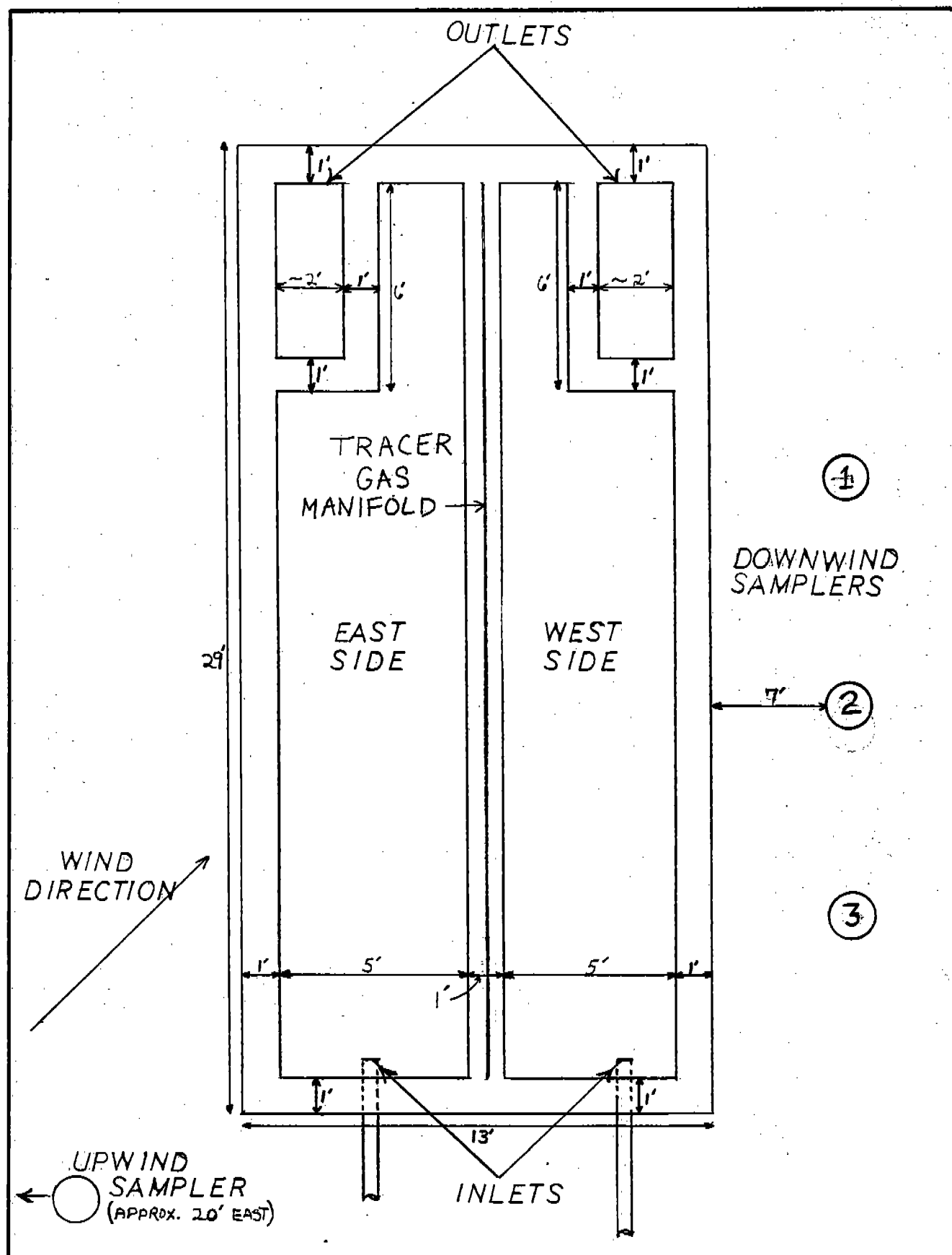
During sampling, the tracer gas manifold was located along the wall separating the two sides of the sump; consequently the emission rate for the entire sump was measured. The average benzene emission rate from the sump was 5.14 lb/hr.

The average benzene concentration in the organic liquid on the surface of the sumps was 27,000 ppm for the west side and 92 ppm for the east side. The concentrations in the aqueous phase which was present at the outlets were 18 and 1 ppm for the respective sides. The outlet samples were dipped from the wells at the south side of the sump, which act as skimmers or weirs by drawing the liquid at the bottom of the sump under the wall into the outlet well.

The average temperature of the liquid in the east sump was 147°F while the average temperature of the west sump was 94°F. In both sumps higher temperatures were measured at the inlets and outlets than in the middle.

The large variations in benzene concentration and temperature found across the surface of the sump suggest non-uniformity in benzene emission rates. The benzene concentration in the surface layer of the west side was 300 times that in the east side. Thus, it would be expected that most of the benzene emissions would come from the west side even though its temperature was 60°F lower than the east side. Both sumps were bottom filled, but there was some turbulence at the inlets. The turbulence





probably caused the highest emissions to occur at the inlet end of the west sump. This is believed to be responsible for the higher emission rates indicated by Sampler 3 in the first three runs (See Table 3-1). During these three runs the air flow was such that Sampler 3 was downwind of the inlet area. Overall, the run to run and sampler to sampler variations are relatively small, and there is every indication that the calculated benzene rates accurately depict the sump's emissions to the atmosphere.



TABLE 3-1  
TRACER DATA  
Republic Steel, Gadsden, Alabama

Sample Loc.	Conc. of Benzene (ppm)	Conc. of Isobutane (ppm)	Mass to Mass Ratio $\phi/ic_4$	Benzene Emission Rate	
				(lb/hr)	(kg/hr)
10/16/80, a.m.					
Test #1, Run #1					
Isobutane release rate: 1.16 lb/hr					
1	4.44	1.71	3.49	4.05	1.84
2	2.19	0.96	3.07	3.56	1.62
3	1.72	0.52	4.49	5.21	2.37
Upwind	0.13	N.D.			
				Avg.	4.27 1.94
10/16/80, a.m.					
Test #1, Run #2					
Isobutane release rate: 1.16 lb/hr					
1	2.62	1.18	3.00	3.48	1.58
2	2.53	1.10	3.07	3.56	1.62
3	3.50	0.85	5.56	6.45	2.93
Upwind	0.14	N.D.			
				Avg.	4.50 2.05
10/16/80, p.m.					
Test #2, Run #1					
Isobutane release rate: 1.15 lb/hr					
1	3.43	1.20	3.85	4.47	2.03
2	3.20	1.30	3.31	3.81	1.73
3	3.48	0.68	6.94	7.98	3.63
Upwind	N.D.	N.D.			
				Avg.	5.41 2.46
10/16/80, p.m.					
Test #2, Run #2					
Isobutane release rate: 1.15 lb/hr					
1	4.58	1.53	4.04	4.65	2.11
2	5.25	1.40	5.05	5.81	2.64
3	3.43	1.03	4.50	5.18	2.35
Upwind	0.44	N.D.			
				Avg.	5.21 2.37





Table 3-1  
(Continued)

Sample Loc.	Conc. of Benzene (ppm)	Conc. of Isobutane (ppm)	Mass to Mass Ratio $\phi/ic_4$	Benzene Emission Rate	
				(lb/hr)	(kg/hr)
10/17/80, a.m.					
Test #3, Run #1					
Isobutane release rate: 1.15 lb/hr					
1	1.86	0.54	4.64	5.34	2.43
2	1.09	0.25	5.96	6.85	3.12
3	4.53	1.01	5.82	6.69	3.04
Upwind	0.61	N.D.			
			Avg.	6.29	2.86
10/17/80, a.m.					
Test #3, Run #2					
Isobutane release rate: 1.14 lb/hr					
1	1.33	0.39	5.20	5.93	2.69
2	2.68	0.91	3.97	4.53	2.06
3	4.74	1.47	4.34	4.95	2.45
Upwind	0.61	N.D.			
			Avg.	5.13	2.60



#### 4.0 PROCESS DESCRIPTION

The light oil intercepting sump is used to collect waste waters from the light oil refining operations. Gravity separates the oil-water waste for reclamation of the light oil. The light oil intercepting sump at Republic Steel in Gadsden, Alabama was open to the atmosphere and was 27 feet long, 11 feet wide and approximately 4 feet deep. The liquid level was approximately three feet below ground level. The sump was divided in half along its length by a wall and was actually two separate sumps, each of which had a separate inlet located on the north side of the sump and an outlet on the south side.



## 5.0 FIELD SAMPLING AND ANALYSIS METHODOLOGY

### 5.1 TRACER GAS METHOD FOR DETERMINATION OF FUGITIVE BENZENE EMISSIONS

The tracer gas method is a practical procedure for quantifying mass emissions of volatile organics from sources which are essentially open to the atmosphere without disturbing flow, dispersion patterns or the source operation. This method utilizes the release of a tracer gas directly over the source of interest; the tracer gas will then follow the same dispersion patterns as the emissions from the source. The mass of tracer released over the sampling period is known and the mass to mass ratio of benzene to the tracer gas in the sample is determined by gas chromatography. The emission rate of the benzene can be calculated with this information.

This method is based on the principle that the chosen tracer gas will model the dispersion of benzene from the source. The tracer gas chosen for this project was isobutane because it was not present in the sources to be tested and it could readily be separated from other source trace components by the same column used for benzene. In addition, isobutane is a non-toxic gas that can readily be dispensed from a pressurized cylinder at a uniform measured rate.

When this method was used triplicate tests were performed. Each test consisted of two 1/2 hour runs. For each run clean and backgrounded ten-liter Tedlar\* bags were used. Integrated samples were collected using Emission Measurements, Inc. Air Quality Sampler II\* systems. The AQS II samplers are self-contained units capable of collecting one or more integrated samples at a preset rate. For tracer tests the sampling rate used was ten liters per hour.

### 5.2 SAMPLE HANDLING

After being collected the gas samples were immediately transported to the gas chromatograph and analyzed. The elapsed time between sample collection and analysis never exceeded one hour. To verify that there was no sample degradation in samples of this type some of the samples were retained for 24 hours and reanalyzed. The loss of benzene and isobutane observed was typically less than 5%.

\*Mention of trade names or specific products does not constitute endorsement by the U.S. Environmental Protection Agency.



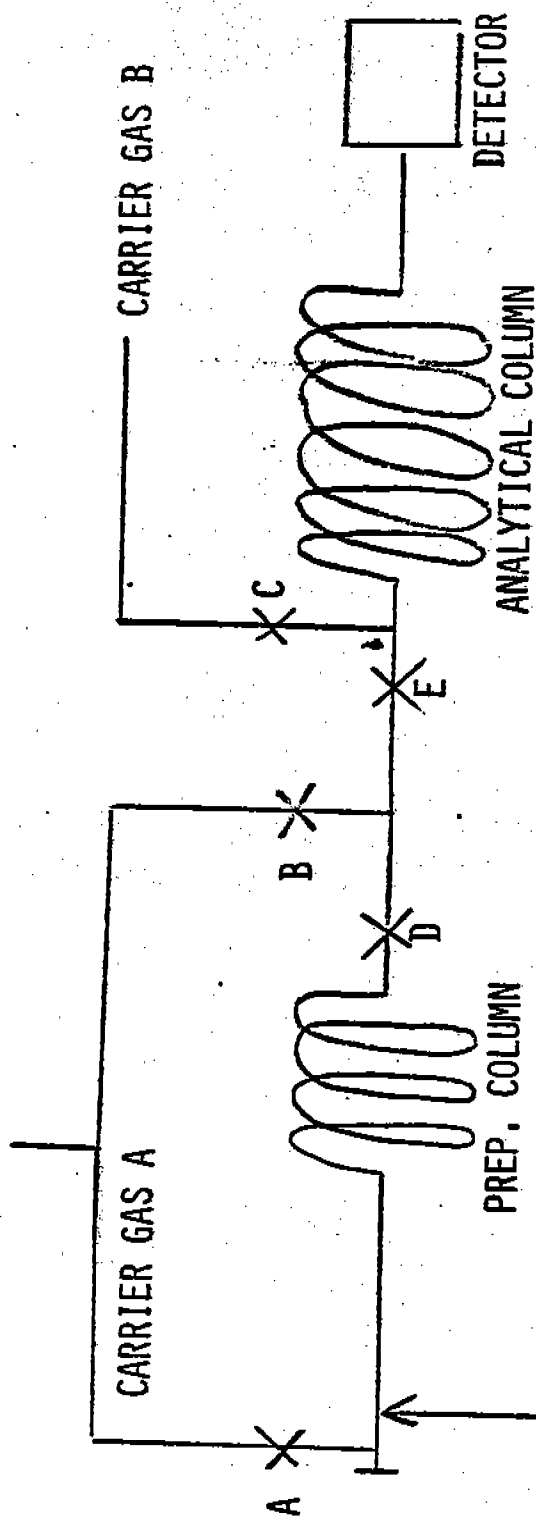
### 5.3 FIELD ANALYSIS

All gas samples collected were analyzed using a Shimadzu GC Mini 1 gas chromatograph equipped with dual flame ionization detectors, dual electrometers, heated sample loop and a backflush system. Figure 5-1 shows a schematic of the backflush apparatus. The backflush system is composed of ten port sequence reversal valve and two columns, a scrubber column for retaining high molecular weight compounds and an analytical column. When the system is in the inject mode the scrubber column and the analytical column are connected in series allowing sample components to move from the precolumn to the analytical column. In the backflush mode the columns are disconnected from each other and become two separate systems each with its own carrier gas source. This arrangement allows the separation and measurement of low molecular weight compounds while the scrubber column is being backflushed of heavier sample components. Backflush times for different mixtures of sample components must be predetermined to insure that the compound(s) of interest are transferred to the analytical column before backflushing is started.

Samples for chromatographic analysis were drawn into a 20 cc glass syringe then introduced to the sample loop inlet. The samples once in the sample loop were allowed to come to atmospheric pressure by waiting 15 seconds prior to the injection. When only benzene was of interest the following chromatographic conditions were maintained:

Column Temperature (isothermal)	- 100°C
Injector and Detector Temperature	- 200°C
5 ml Sample Loop, Temperature	- 50°C
Carrier Gas Flow Rate	- 32 cc/min
Hydrogen Flow Rate	- 40 cc/min.
Air Flow Rate	- 240 cc/min.
Analysis Time	- 5 min.
Detector	- Flame Ionization





SAMPLE INJECTION

INJECT

A, D, E OPEN

B, C CLOSED

BACKFLUSH

A, E CLOSED

B, C, D OPEN

GC COLUMN CONFIGURATION WITH BACKFLUSH

The columns used for field analysis were:

A - Scrubber Column

10% FFAP on Supelcoport 80/100  
1/8" x 1 m Stainless Steel

B - Analytical column

20% SP-2100, 0.1% Carbowax 1500  
100/120 Supelcoport  
1/8" x 10' Stainless Steel

When samples from tracer tests were analyzed the chromatographic conditions were changed to provide adequate separation of the isobutane tracer from the other light components of the sample. The temperature program used for this analysis was:

- 1) Start at room temperature with external cooling fan on and oven door open.
- 2) Inject @ 0.0 min.
- 3) Turn external cooling fan off @ 1.0 min.
- 4) Backflush @ 1.8 min.
- 5) Isobutane elutes @ 2.3 min.
- 6) Close oven door @ 3.0 min. with oven temperature set at 100°C.
- 7) Benzene elutes @ 7.0 min.
- 8) After the elution of benzene, open the oven door and turn on the cooling fan. The next injection can be made after 2 minutes of cooling.
- 9) When the tracer gas is used analysis time will be approximately 10 minutes.

The columns and flow rates were the same as for isothermal.



## 6.0 FIELD SAMPLING PROCEDURES

### 6.1 LIGHT OIL INTERCEPTING SUMP

The sump was a fugitive emission source which was sampled using the tracer gas method. When using this method, best results are obtained by releasing the tracer gas at the liquid surface level along the central axis of the source perpendicular to the wind direction. This was accomplished for this source by placing the dispersion bar on the wall which separated the east and west sides of the sump, as depicted in Figure 3-1. The wall ran north and south and was approximately 4-6 inches above the liquid level of the sump. The tracer gas source was connected to the center of the 27 foot long dispersion bar which was comprised of six 4 1/2 foot sections joined by Swagelok connectors. On each side of the dispersion bar the holes in the bar were 19 inches apart and were of increasing size outward from the tracer source. The first section contained holes that were 0.166 inches in diameter, the second section contained holes 0.169 inches in diameter and the third section had holes that were 0.173 inches in diameter. Visual inspection of the dispersion bar at release rates typically used for testing showed that approximately the same volume of gas was exiting the holes in various sections of the bar.

Three samplers were positioned 7 feet from the sump on its west side and the presence of isobutane and benzene at the sampler locations was verified by analyzing grab samples. The upwind sampler was positioned approximately 20 feet from the sump's northeast corner.



## 7.0 LABORATORY SAMPLE ANALYSIS

Two types of liquid samples were collected: process liquids, and sample line and water trap catches and washes. All liquid samples were stored in amber glass bottles and returned to Scott's Plumsteadville laboratory for analysis.

### 7.1 SAMPLE PREPARATION

Depending upon the complexity of the sample, one of the following sample preparation procedures was followed prior to the "purge and trap" procedure and analysis.

#### Samples Containing Immiscible Liquid Phases

Using a clinical centrifuge (International Equipment Company, Massachusetts) immiscible liquid phases were separated and each phase was analyzed separately for benzene.

#### Samples Containing Solid and Immiscible Liquid Phases

Samples containing solids of higher density than the liquid phase were separated by centrifuge or by simple decantation of the liquid. The different phases in the liquid fraction were then further separated by centrifuging. Solid and liquid phases were analyzed separately.

#### Samples Containing Finely Crystalline Solid Suspension

In analyzing these samples the stoppered sample jars were shaken for at least half an hour for homogenizing the solution. The uniform distribution of suspended fine crystalline solid particles was tested by determining the percentage of dry solid in several aliquots of the homogenized mixture. A weighed amount of the mixture was analyzed for benzene.





### Sampling System Washings

All washings were clear solutions having only one liquid phase. The total weight of the liquid phase was determined using a balance correct to  $\pm 0.1$  g. The total weight of each washing was more than 25 grams, so an error of 0.1 g in weighing the mass will contribute an error of only 0.4% to the final analytical data. A weighed aliquot of the washing was analyzed for benzene by following the "purge and trap" and analysis procedures outlined in the following sections, and using this analysis data the weight of benzene present in the total mass of washing was calculated.

### 7.2 PURGE AND TRAP PROCEDURE FOR EXTRACTION OF BENZENE FROM LIQUID PHASE TO GASEOUS PHASE

An accurately weighed quantity of the sample to be analyzed was diluted with 20-25 ml of propylene carbonate in a specially designed glass purging apparatus which was kept immersed in a thermostatted water bath maintained at 78°C. Benzene free nitrogen gas was bubbled through the propylene carbonate solution in the purging apparatus at the rate of 0.2 - 0.3 liters/minute, and collected in leak free Tedlar bags. Under these experimental conditions, 1 1/2 - 2 hours were sufficient to purge off all the benzene from the liquid phase to the gaseous phase. The total volume of nitrogen gas used to purge the sample was accurately measured by a calibrated dry gas meter. A diagram of the purge and trap set-up is shown in Figure 7-1.

Propylene carbonate was found to be an ideal diluting solvent for the extraction of benzene from all types of liquid samples containing viscous tar, pitch, light and heavy oil and insoluble particulates. It was chosen for its high boiling point, low density, and good solvating capacity.



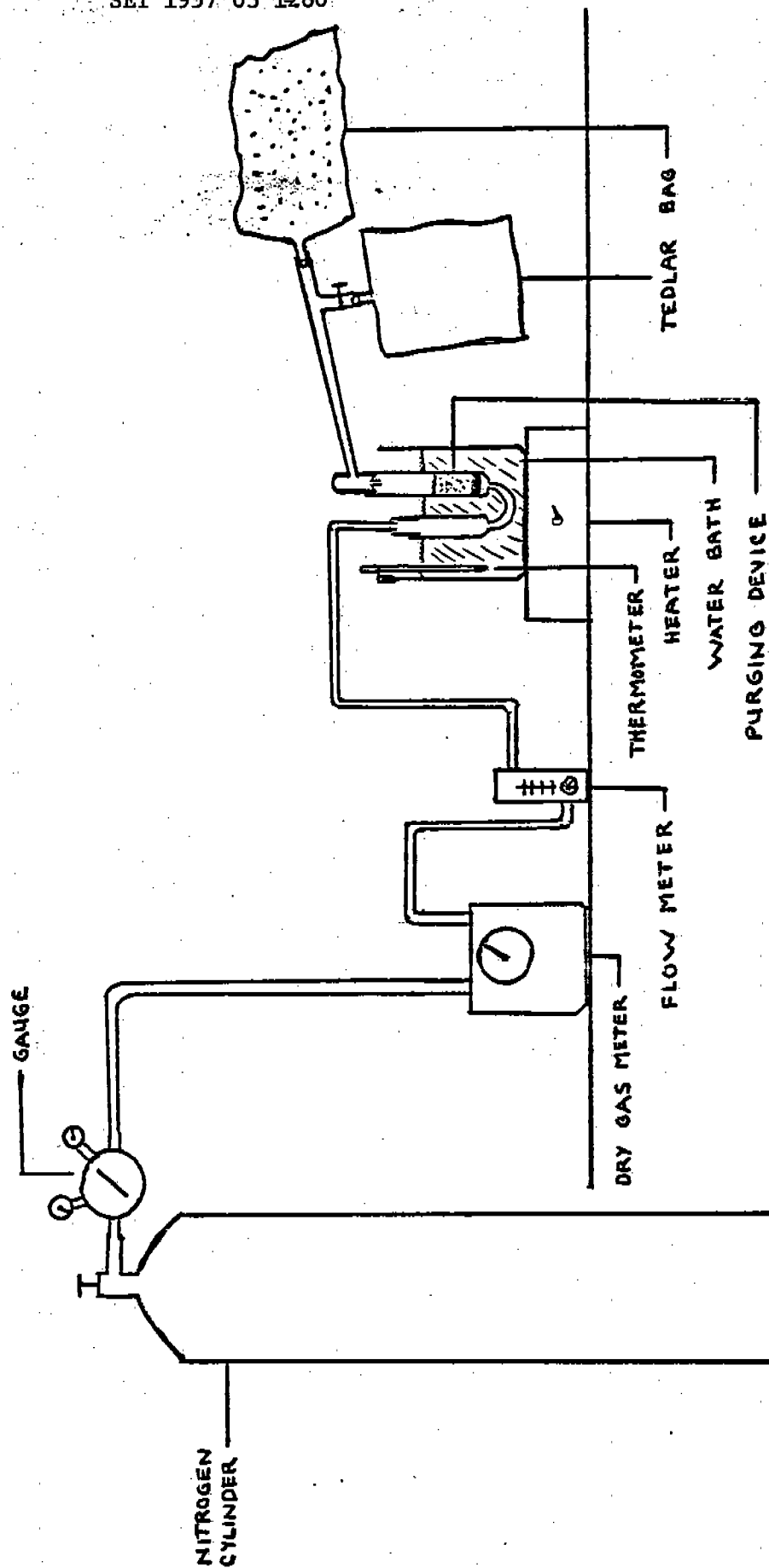


FIGURE 7-1 PURGE AND TRAP METHOD EQUIPMENT SET-UP

### 7.3 GAS CHROMATOGRAPH

A Perkin-Elmer 900 gas chromatograph was used for the analysis of the purge bags. A 10 ft. by 1/8 inch stainless steel column packed with 20% SP-2100/0.1% Carbowax 1500 on 80/120 mesh Supelcoport was used for the analysis. This column gave complete resolution of the benzene peak from other components present in the purge bags. The 'peak height' method was utilized to calculate the concentration of benzene in the purge bags analyzed. The Perkin-Elmer 900 used for analysis was not equipped with a backflushing unit. Gas chromatograph conditions were as follows:

GC column temperature: 70°C isothermal

Detector temperature: 190°C

5 ml loop at a temperature of 120°C

Carrier gas flow rate: 30 cc/min He

Hydrogen flow rate: 45 cc/min

Oxygen flow rate: 400 cc/min

Detector: Flame Ionization Detector (FID)

In addition to benzene, the purge bags contained other volatile hydrocarbons present in the liquid samples such as toluene and naphthalene. Because this chromatograph was not equipped with a backflush, it was necessary to elute all heavy organics from the column by heating the column to 150°C after every two injections for one hour with the carrier gas on. After cooling the column to 70°C the absence of any organic in the column which might overlap the benzene peak in the next analysis was checked. When the column was found to be satisfactorily clean, the next analysis was continued under the conditions previously described.



### 8.0 QUALITY CONTROL AND QUALITY ASSURANCE

The following sections will address quality control and quality assurance procedures for the field analysis of benzene in air samples and the laboratory analysis of process liquids and BaP samples.

#### 8.1 FIELD ANALYSIS PROCEDURES

All samples were analyzed in duplicate and as a rule peak heights were reproduced to within 5%. For some very high concentration samples (percent range) it was necessary to make dilutions for analysis. When this was done a fresh dilution was prepared for each injection and peak heights were reproduced to within 10%. To verify that the system was retaining no benzene, frequent injections of the standard and nitrogen were made. In all cases the result was satisfactory.

The Tedlar bags that were reused for sampling were flushed three times with nitrogen and allowed to sit overnight after being filled to approximately three quarters of their capacity. They were analyzed for benzene content the following day. The background concentrations of the bags were recorded and varied from 0 to 10 ppm benzene. Care was taken to use sample bags whose background concentration was very low compared to the expected concentration of the source.

The accuracy and linearity of the gas chromatographic techniques used in this program were tested through the use of EPA Audit Samples. Two standards, a 122.5 ppm and 6.11 ppm benzene were used to analyze the audit cylinders.



## 8.2 PROCEDURES FOR ANALYSIS OF PROCESS LIQUIDS

Scott's benzene standards, checked against EPA Audit Standards, were used as reference standards throughout this program. The accuracy and linearity of the gas chromatographic technique for benzene analysis was tested through the use of EPA Audit Standards which were available to Scott. Gas chromatographic analysis of the samples and standard were performed under identical conditions to assure the accuracy of the analytical data generated.

Each batch of propylene carbonate which was used as the diluting solvent in the purge and trap technique was analyzed for benzene content by subjecting 25 ml of propylene carbonate to the purge and trap procedure followed by gas chromatographic analysis of the trapped gas under identical conditions as described in Section 5.2. All batches of analytical grade propylene carbonate were found to be free from benzene.

Every day before the analysis of samples the purging apparatus and trapping bags were tested for absence of benzene. Whenever the whole system was found to be free from benzene to the lowest detectable limit of the instrument, the samples were analyzed using the purging apparatus and the trapping gas sampling bags.

Generally an accurately weighed mass of each sample was subjected to purge and trap procedure only once and the trapped gas sample was repeatedly analyzed by GC until the analytical data of consecutive GC analyses varied by  $\pm 0.5\%$  or less.



For randomly selected samples, the whole analytical procedure was repeated with a different weighed mass of the source sample to check the validity and accuracy of the analytical methodology. The analytical data for different runs were found not to vary by more than 5%.

By purging the sample with nitrogen under the experimental conditions as utilized by Scott, the recovery of benzene from the sample was quantitative and this has been verified by analyzing a standard benzene solution in propylene carbonate containing tar and pitch.



APPENDIX A  
SAMPLE CALCULATIONS



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APPENDIX A  
SAMPLE CALCULATIONS

Example: Test 1, Run 1, Sampler 1

Concentration of benzene: 4.44 ppm  
Concentration of isobutane: 1.71 ppm  
Isobutane release rate: 1.16 lb/hr.

Calculation of Mass to Mass Ratios:

Benzene 4.44 ppm X 78 g/mole = 346.32

Isobutane 1.71 ppm X 58 g/mole = 99.18

$\frac{346.32}{99.18} \times 1.16 \text{ lb/hr.} = 4.05 \text{ lb/hr. benzene}$





APPENDIX B  
FIELD DATA SHEETS



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PROJECT 1922

TRACER GAS DATA SHEET

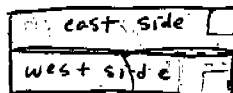
Page B-1

PLANT: Republic, GadsdenDATE: 10/16/80PROCESS: SumpWIND SPEED: light

PROCESS NOTES:

WIND DIRECTION: east

4) ↑  
upwind



tracer bar

WIND  
↓

AMBIENT TEMPERATURE: \_\_\_\_\_

BAROMETRIC PRESSURE: \_\_\_\_\_

Sampler Number

Distance from Source

Sampling Rate

Pump Numbers

Tedlar bag numbers

Start Time

Stop Time

DOWNWIND						UPWIND	
1		2		3		4	
7 ft		7 ft		7 ft		20 ft	
10 lph		10 lph		10 lph		10 lph	
5		10		8			
1	5	2	6	4	7	3	8
8:30	9:05	8:30	9:05	8:30	9:05	8:35	9:05
9:00		9:00		9:00		9:00	

Gas meter  $\gamma = 1.059$ 

ISOBUTANE RELEASE: Gas Temperature

TIME	METERED VOLUME	
8:30	0	244.050
	2	244.302
	4	244.550
	6	244.795
	8	245.038
	10	245.281 .123
	12	245.642
	14	245.763
	16	246.030
	18	246.240
	20	246.472 .119
	22	246.704
	24	246.943
	26	247.194
	28	247.442
	30	247.692 .122

Gas Pressure

TIME	METERED VOLUME	
9:05	0	248.325
	2	248.578
	4	248.832
	6	249.082
	8	249.332
	10	249.579 .125
	12	249.827
	14	250.074
	16	250.315
	18	250.555
	20	250.887 .131
	22	251.025
	24	251.261
	26	251.492
	28	251.720
	30	251.951

Samplers about 4 feet apart, 7 ft. from railing of sump.

$$3.642 \text{ ft}^3/30 \text{ min} = .1214 \text{ cfm}$$

$$\times 1.059$$

$$0.1286 \text{ cfm}$$

$$3.626 \text{ ft}^3/30 \text{ min} = 0.1209 \text{ cfm}$$

$$\times 1.059$$

$$0.1280 \text{ cfm}$$

PROJECT 1922

## TRACER GAS DATA SHEET

PLANT: Republic-Gadsden AlaDATE: 10/16/80PROCESS: SumpWIND SPEED: light

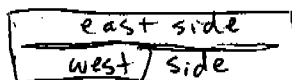
PROCESS NOTES:

WIND DIRECTION: east

AMBIENT TEMPERATURE: \_\_\_\_\_

BAROMETRIC PRESSURE: \_\_\_\_\_

liquid  
~ 4 ft deep.  
West side has  
~ 1 ft sludge  
on bottom



WIND  
↓

Sampler Number

Distance from Source

Sampling Rate

Pump Numbers

Tedlar bag numbers

Start Time

Stop Time

DOWNWIND						UPWIND	
1	2	3	4				
7 ft	7 ft	7 ft	~ 20 ft				
10 lph	10 lph	10 lph	10 lph				
9	13	10	14	11	15	12	3
9:40	11:02	9:40	11:02	9:40	11:02	9:40	11:02

Gas meter  $\gamma = 1.059$ 

## ISOBUTANE RELEASE: Gas Temperature

TIME	METERED VOLUME
9:40	0
2	252.460
4	252.686
6	252.935
8	253.182
10	253.429
12	253.672 .121
14	253.917
16	254.158
18	254.400
20	254.640
22	254.877 .1205
24	255.109
26	255.338
28	255.573
30	255.822
	256.072

## Gas Pressure

TIME	METERED VOLUME
11:02	0
2	260.210
4	260.451
6	260.702
8	260.949
10	261.197
12	261.437 .1227
14	261.670
16	261.899
18	262.132
20	262.361
22	262.590 .116
24	262.832
26	263.086
28	263.338
30	263.581
	263.830

$$3.612 \text{ ft}^3/30 \text{ min} = .1204 \text{ cfm}$$

$$\times 1.059 = .1275 \text{ cfm}$$

~~0.1275 cfm~~

$$3.620 \text{ ft}^3/30 \text{ min} = .1206 \text{ cfm}$$

$$\times 1.059$$

0.1277 cfm

PROJECT 1922

TRACER GAS DATA SHEET

PLANT: Republic - Gadsden, Alabama

DATE: 10/16/80

PROCESS: Lt. oil sump

WIND SPEED: light

PROCESS NOTES:

WIND DIRECTION: east

inlet end on east side is bubbling  
west side very sludgy

AMBIENT TEMPERATURE:

BAROMETRIC PRESSURE:

Sampler Number

Distance from Source

Sampling Rate

Pump Numbers

Tedlar bag numbers

Start Time

Stop Time

DOWNWIND						UPWIND	
1	2	3	4				
7 ft	7 ft	7 ft	~ 20 ft				
10 lph	10 lph	10 lph	10 lph				
1/3	1	1/2	2	3/4	4	8	
1:30	2:05	1:30	2:05	1:30	2:05	1:30	
2:00	2:35	2:00	2:35	2:00	2:35	2:35	

Gas meter  $V = 1.059$ 

ISOBUTANE RELEASE: Gas Temperature

TIME	METERED VOLUME	
1:30	0	264.510
	2	264.758
	4	264.998
	6	265.230
	8	265.456
	10	265.689 .118
	12	265.932
	14	266.175
	16	266.424
	18	266.664
	20	266.900 .119
	22	267.144
	24	267.395
	26	267.642
	28	267.888
	30	268.131

Gas Pressure

TIME	METERED VOLUME	
2:05	0	268.800
	2	269.045
	4	269.299
	6	269.545
	8	269.788
	10	270.026 .1226
	12	270.262
	14	270.497
	16	270.722
	18	270.949
	20	271.162 .114
	22	271.404
	24	271.657
	26	271.902
	28	272.148
	30	272.389

$$3.621 \frac{ft^3}{30 \text{ min}} = .1207 \text{ cfm}$$

$$\times 1.059$$

0.1278 cfm

$$3.589 \frac{ft^3}{30 \text{ min}} = .1196 \text{ cfm}$$

$$\times 1.059$$

0.1267 cfm

SAMPLE DATAPlant Republic-Gadsden Ala Process Sump Date 10/16/80Sample No. west side inlet Time Sampled \_\_\_\_\_Sample Type: Liquid AirSample Temperature 87°F

Ambient Temperature \_\_\_\_\_

Description of Sampling Location:

Sample No. west side middle Time Sampled \_\_\_\_\_Sample Type: Liquid AirSample Temperature 82°F

Ambient Temperature \_\_\_\_\_

Description of Sampling Location:

Sample No. west side outlet Time Sampled \_\_\_\_\_Sample Type: Liquid AirSample Temperature 114°F

Ambient Temperature \_\_\_\_\_

Description of Sampling Location:



S A M P L E   D A T APlant Republic-Gadsden Abc Process Sump Date 10/16/80Sample No. East side inlet Time Sampled 11:35Sample Type: Liquid AirSample Temperature 146 °F

Ambient Temperature \_\_\_\_\_

Description of Sampling Location:

Sample No. east side middle Time Sampled 11:37Sample Type: Liquid AirSample Temperature 139 °F

Ambient Temperature \_\_\_\_\_

Description of Sampling Location:

Sample No. east side outlet Time Sampled 11:40Sample Type: Liquid AirSample Temperature 156 °F

Ambient Temperature \_\_\_\_\_

Description of Sampling Location:



Scott Environmental Technology Inc.

APPENDIX C  
LABORATORY DATA SHEETS



Scott Environmental Technology Inc.

## CHROMATOGRAPHIC ANALYSIS LOG

Reg. Cite. Soil, Sediment, H/La.

Project No. 1957

Date 9/6/80

Analyst TB

Time	Sample Identification	Peak Height/Area	Concentration Factor	Concentration	Comments
12.9	Std. Cal. 11 $100 \mu\text{g}$ $64 \times 10^4$ - 100 $\mu\text{g}$	5975 110	0.102 0.096		
	Test #1, Run #1, Bag #1 Direct - $32 \times 10^4$ # - $64 \times 10^4$	35.5 43.5	0.048 <del>0.048</del> 0.102	<del>1.74</del> <del>1.74</del> $\times 58 =$ $444 \times 78$	Freezing <del>318</del> 9918 > 349 (S) 34632
	Test #1, Run #1, Bag #2 Direct - $64 \times 10^4$ # - $64 \times 10^4$	10 215	0.096 <del>0.096</del> 0.102	$0.96 \times 58 =$ $219 \times 78 =$	5568 > 307 (17) 17082
	Test #1, Run #1, Bag #4 Direct - $16 \times 10^4$ # - $64 \times 10^4$	215 69	0.024 0.026	$0.52 \times 58$ $1.72 \times 78$	2993 > 1419 (15) 13455
	Test #1, Run #1, Bag #3 Direct - $16 \times 10^4$ # - $64 \times 10^4$	5 110	0.026	0.1316	





## CHROMATOGRAPHIC ANALYSIS LOG

Project No. 1957

Date 10/1/80

Analyst TB

Republic Steel Madison  
Ala.

Time	Sample Identification	Peak Height/Area	Concentration Factor	Concentration	Comments
	Republic Steel 60" x 4 - 64x10 <sup>4</sup> 106 ppm Cu - 32x10 <sup>4</sup>	62.5 22.5	0.099 0.017		Average = 3.88
	Test #1, Run #2 Bag #5 Ac-Cu - 64x10 <sup>4</sup> φ - 64x10 <sup>4</sup>	26 12.5	<del>0.050</del> 0.099 <del>0.047</del> 0.094	1.18 <del>2.62</del> x 58 #18 162 x 78	6.815 204.36 > 300
	Test #1, Run #2 Bag #6 Ac-Cu - 32x10 <sup>4</sup> φ - 32x10 <sup>4</sup>	<del>50.5</del> 50.5 23.5	0.050 0.047	<del>2.53</del> 1.10 x 58 #10 153 x 18	6406 196.95 > 307
	Test #1, Run #2 Bag #7 Ac-Cu - 32x10 <sup>4</sup> φ - 32x10 <sup>4</sup>	70 18	0.050 0.047	0.85 x 58 3.50 x 18	4907 273.0 > 5.56
	Test #1, Run #2 Bag #8 Ac-Cu - 8x10 <sup>4</sup> φ - 8x10 <sup>4</sup>	10 11	0.013	0.14 ppm	A



## CHROMATOGRAPHIC ANALYSIS LOG

Bridgeton, NJ

Project No. 1957

Date 9/12/90

Analyst TBS

Time	Sample Identification	Peak Height/Area	Concentration Factor	Concentration	Comments
	Bag 1 8x10 <sup>4</sup>	9 - 6	.012	.108	
	Bag 2 8x10 <sup>4</sup>	7 - 4	.012	.084	
	Bag 3 8x10 <sup>4</sup>	5 - 6	.012	.060	
	Bag 1	4 - 3	.012	.036	
	Bag 2	4 - 10	.011	.11	
	Bag 1	4 - 2	.012	.034	
	Bag 2	4 - 8	.011	.088	
	Bag 1	4 - 10	.012	.12	
	Bag 2	4 - 12	.011	.132	



## CHROMATOGRAPHIC ANALYSIS LOG

Republic Steel, Dockland Area

Project No. 1957

Date 10/1/80

Analyst TR

Time	Sample Identification	Peak Height/Area	Concentration Factor	Concentration	Comments
	Frozen Steel KC4 - 32x10 <sup>4</sup> - 106 ppm φ - 64x10 <sup>4</sup> - 611 ppm	21 59	.050 .104		Average = 4.70
	Test #2 Run #1 Bag #9 KC4 - 64x10 <sup>4</sup> φ - 64x10 <sup>4</sup>	12 33	.100 .104	12x58 = 343x78 =	696 > 3.85 26730
	Test #2 Run #2 Bag #10 KC4 - 32x10 <sup>4</sup> φ - 52x10 <sup>4</sup>	26 61.5	.050 .052	13x58 = 320x78 =	75.4 > 3.31 249.44
	Test #2 Run #1 Bag #11 KC4 - 32x10 <sup>4</sup> φ - 32x10 <sup>4</sup>	135 67	.050 .052	0.68x58 = 348x78 =	39.5 > 6.94 271.75
	Test #2 Run #1 Bag #12 KC4 16x φ 16x	110 3			



## CHROMATOGRAPHIC ANALYSIS LOG

Project No. 1757 Date 10/10/90 Analyst TBS



Scott Environmental Technology Inc.

Time	Sample Identification	Peak Height/Area	Concentration Factor	Concentration	Comments
	Trace Steel				
	6.11 ppm $\phi$ - 64x10 <sup>4</sup>	59.5			
	1006 ppm $\phi$ - 32x10 <sup>4</sup>	21			
	Test #2 Run #2 Bag #14				
	64 $\phi$ 32x10 <sup>4</sup>	30.5	05	153x58 =	3845 > 4104
	$\phi$ - 64x10 <sup>4</sup>	44	.104	458x78	35693
	Test #2 Run #2 Bag #13				
	64 $\phi$ 32x10 <sup>4</sup>	14	.10	14x58	812 > 505
	$\phi$ - 64x10 <sup>4</sup>	50.5	.104	525x78	40966
	Test #2 Run #2 Bag #15				
	64 $\phi$ 32x10 <sup>4</sup>	20.5	005	103x58 =	5945 > 450
	$\phi$ - 64x10 <sup>4</sup>	33	0.104	343x78 =	26770
	Std				
	6.11 ppm $\phi$ - 64x10 <sup>4</sup>	62			
	1006 ppm $\phi$ - 32x10 <sup>4</sup>	22			
	Test #2 Run #2 Bag #13				
	64 $\phi$ 32x10 <sup>4</sup>	ND	.026		
	$\phi$ - 64x10 <sup>4</sup>	17		.44	

Average 453

Project No. 1957

**Date**

10/7/01

**Analyst**

Time	Sample Identification	Peak Height/Area	Concentration Factor	Concentration	Comments
	Unknown Std. Cell type: $\phi$ - $64 \times 10^4$ MCy - $32 \times 10^4$	58 215	0.105 0.049		Average - 5.47
	Tail #3 Run #1 Bag #12 $\phi$ - $32 \times 10^4$ <del>MCy</del> - $32 \times 10^4$	11 355	0.019 0.053	$0.54 \times 58 =$ $1.86 \times 78 =$	3132 > 4.64 145.37
	Tail #3 Run #1 Bag #13 $\phi$ - $32 \times 10^4$ MCy - $32 \times 10^4$	205 5	0.053 0.049	$1.09 \times 78 =$ $0.25 \times 58 =$	84.78 > 5.94 14.21
	Tail #3 Run #1 Bag #14 $\phi$ - $32 \times 10^4$ MCy - $32 \times 10^4$	82 205	0.053 0.049	$4.63 \times 78 =$ $1.01 \times 58 =$	338.98 > 5.82 58.26
	Reagent Water #1 Stability $\phi$ $32 \times 10^4$ MCy $32 \times 10^4$	55 12	0.053 0.049	$2.92 \times 78 =$ $0.58 \times 58 =$	227.37 > 6.66 34.16



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## CHROMATOGRAPHIC ANALYSIS LOG

Project No. 1957

Date 10/17/80

Analyst TS



Scott Environmental Technology Inc.

Page C-7

Time	Sample Identification	Peak Height/Area	Concentration Factor	Concentration	Comments
	Feed #3 Run #2 Bag #1 164 - 32x10 <sup>4</sup> φ - 32x10 <sup>4</sup> Treated Steel 611 φ - 64x10 <sup>4</sup> 106 φ - 32x10 <sup>4</sup>	7 25 58 21	.049 <del>.053</del>  .053	0.31 x 58 = 1.33 x 78 =	19.89 > 5.20 103.35
	Feed #3 Run #2 Bag #2 164 - 32x10 <sup>4</sup> φ - 32x10 <sup>4</sup>	18.5 50.5	.049 .053	0.91 x 58 = 2.68 x 78 =	52.58 > 3.97 208.77
	Feed #3 Run #2 Bag #4 164 - 32x10 <sup>4</sup> φ - 32x10 <sup>4</sup>	30 89.5	.049 .053	1.47 x 58 = 4.74 x 78 =	85.20 > 4.34 369.94
	Requart Run #6 Steel Bag 164 - 32x10 <sup>4</sup> φ - 32x10 <sup>4</sup>	23.5 50.5	.049 .053	1.15 x 58 = 2.68 x 78 =	66.70 > 3.13 209.04
	Requart Run #15 Steel Bag 164 - 32x10 <sup>4</sup> φ - 32x10 <sup>4</sup>	14	.049	1.37 x 58 =	79.58

## CHROMATOGRAPHIC ANALYSIS LOG

Project No. \_\_\_\_\_

Date \_\_\_\_\_

Analyst \_\_\_\_\_

Time	Sample Identification	Peak Height/Area	Concentration Factor	Concentration	Comments
	Trace in Std 6.11 gpm $\phi$ - $6.1 \times 10^4$ 1.06 gpm ACY - $3.2 \times 10^4$	61 23			
	Trace in 13 Run #2 Bag ACY - $8 \times 10^4$ $\phi$ - $8 \times 10^4$	110 46	0.013	0.61	
	Std 132.5 gpm $128 \times 10^3$ 130° Doo				
	Sub C Sample Inlet $128 \times 10^3$				
	Sub C Sample Inlet Don Sudo				



APPENDIX D  
TRACER GAS METHOD DEVELOPMENT



Scott Environmental Technology Inc.



## APPENDIX D

## TRACER GAS METHOD DEVELOPMENT

D.1 Tracer Gas Selection

The initial consideration when using the tracer gas method is the choice of a suitable gas. There are several criteria used in the selection: First, the tracer gas must not be present in the atmosphere at the sampling location. Second, the tracer gas must be separable from other components in the background at the sampling location and quantifiable on the same GC column without interfering with the elution of the compound(s) of primary interest. The tracer gas should also be readily available, transportable, economically feasible, and safe for the given usage situation.

For the determination of benzene emissions at secondary by-products plants, isobutane is the recommended tracer gas. The second choice for a tracer gas is a halogenated hydrocarbon. At secondary by-products plants the hydrocarbons in the background atmosphere are almost exclusively emissions from the coking operation and neither isobutane nor halogenated hydrocarbons are present to any significant degree. Isobutane was chosen over a halogenated hydrocarbon on the basis of chromatographic elution characteristics. Isobutane elutes well before the benzene peak thus eliminating any interference when using a temperature program for the chromatographic analysis.

The separation of isobutane from mixtures containing concentrations of hydrocarbons typical of secondary by-products plants was verified by spiking samples collected at different sources in a secondary by-products plant with various concentrations of isobutane and performing

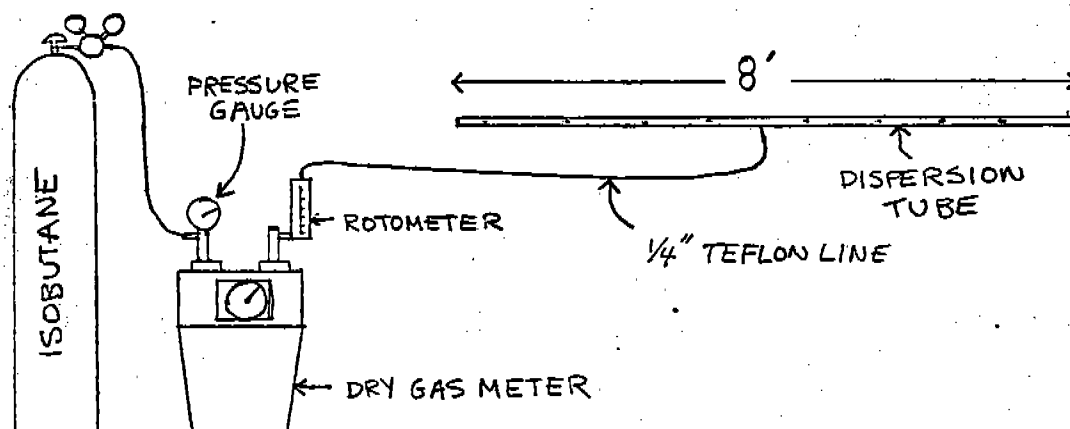


a temperature program of chromatographic analysis to achieve the desired degree of separation. In all cases the desired separation was achieved.

#### D-2 Dispersion Apparatus

The apparatus for the dispersion of tracer consists of a cylinder of the tracer gas connected to a dry gas meter, a rotameter and a dispersion tube. All necessary connecting lines are Teflon.

Two different dispersion tube configurations were tested, both were constructed from 1/4" O.D. stainless steel tubing. The first tube tested was 8' long with the tracer source connected to one end of the tube. The tube contained holes every 19" which were progressively larger moving away from the gas source. The hole size ranged from 0.062" to 0.031". The second tube was 8' long in two 4' sections which are connected via a T-joint to each other and to the tracer gas source. This dispersion tube has 0.041" holes every 19" and the ends are capped.

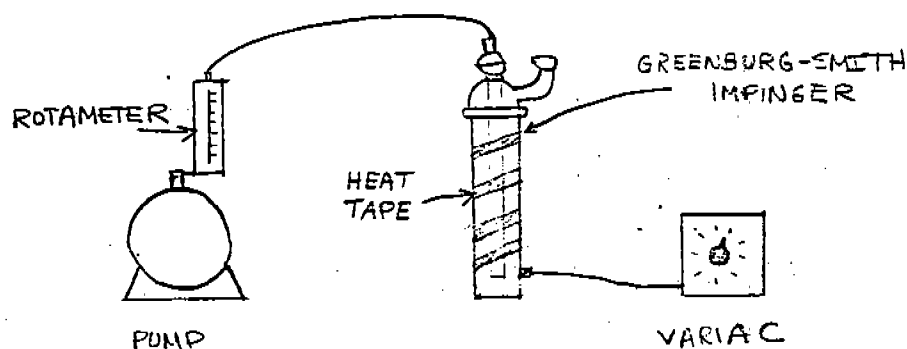


Of the two types of dispersion tubes tested the latter described was more efficient for the dispersion of the tracer. This judgement was made by visual inspection of the holes in each tube while isobutane was flowing at



0.1 CFM. At this rate isobutane can be seen as it leaves the dispersion tube and differences in the relative volume leaving each hole are visually discernible. The first configuration had all gas coming out of the first 2 holes, whereas the second configuration had uniform emissions from each orifice.

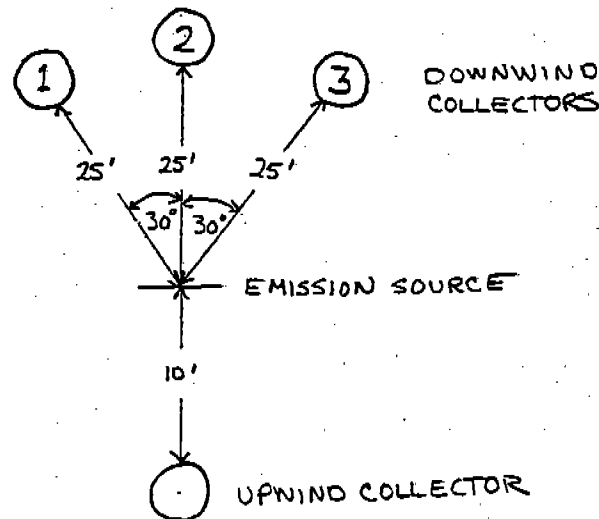
Benzene was also released in two ways; by evaporation and a heated bubbler. Both methods proved adequate for experimental determinations. When evaporation was used to release benzene, a stainless steel pan 16" x 24" x 1/2" was employed to contain the benzene. During an experimental determination benzene was added to the pan in 50 cc aliquots at intervals frequent enough to maintain a constant surface area of benzene. This was done in order to keep the emission of benzene at a constant rate. However, this evaporation method proved unsatisfactory on days when the wind speed exceeded 15-20 MPH due to the changing evaporation rate resulting from gusting wind. A more steady emission of benzene was achieved by using a heated bubbler. The bubbler system consisted of a 500 cc impinger of the Greenburg-Smith design wrapped with a heat tape. The impinger was kept at a constant temperature below the boiling point of benzene. A rubber diaphragm pump was used to push atmospheric air through a bubbler. Flow was regulated with a rotameter.



It was necessary to add more benzene during an experimental run, because the emission rate drops substantially if the benzene level drops too low in the impinger. The frequency of addition and the quantity of benzene per addition are dependent on the emission rate being used. For our determinations it was necessary to add 50 cc of benzene at intervals of approximately 10 minutes.

### D-3 Experimental Determinations

An experiment consists of the release of a known amount of isobutane and benzene simultaneously. Samples are collected along a  $30^\circ$  arc, 25 feet downwind from the source of the emissions.



Initially samples were grab samples collected in clean one liter glass gas flasks. Later samples were integrated over a 1/2 hour period and collected in clean 10-liter Tedlar bags via Emission Measurements Air Quality Sampler with a flow rate of 10 LPH.

In initial determinations, portions of actual presurvey samples containing 62% benzene were released in an effort to simulate



the type of sample which would be encountered in the field. Various amounts of the sample mixture from 0.20 to 10 cc were released and samples were collected downwind in 1-liter gas flasks. When these samples were analyzed the amount of benzene detected was very small, approximately 20 ppb. From this it was apparent that it would be necessary to release significantly more benzene in order to produce the necessary concentration at the sampling location so that quantitative mass to mass ratios could be calculated.

Because of the necessity of releasing more benzene and avoiding the foul odor which the high concentration benzene field samples possessed, it was decided that pure benzene be used for all subsequent determinations.

For the next series of experiments evaporation as previously described was used to release benzene. This series of experiments produced results accurate to within 10% of the theoretical mass to mass ratios with a minimum benzene emission of 0.54 lb/hr for the series. These experiments were performed on days when the wind speed was light (5 - 10 MPH) and the wind direction was steady (See Table D-1).

The next experiment was designed to test the variations which might be introduced when the wind speed and direction were less than favorable. On the day selected the wind speed was 20-25 MPH and the direction was 180° variable due to a changing weather system. The rate of evaporation of the benzene was noticeably affected by the conditions as were the dispersion patterns of the emissions. Erratic results were produced by the meteorological stress on key experimental variables. Calculated mass to mass ratios differed from the theoretical value from 15% to as much as 56%, demonstrating the effect of high and variable winds on the technique. In order to reduce stress on the experiment the benzene bubbler as described was used to provide



a steady source of benzene emission at a rate that would be independent of meteorological conditions. On the day chosen to use the bubbler system the wind speed was 15-20 MPH and the direction was steady. Favorable results were obtained despite the relatively strong wind demonstrating that the tracer technique is valid in winds up to 20 MPH depending on the sampling location (see Table D-1).

#### D-4 Summary

When using the tracer gas method it is necessary to verify that the tracer gas is detectable at the sampling location of choice as the method is somewhat dependent upon meteorological conditions. The method works best when the wind speed is light to moderate, 5-15 MPH, and the wind direction is steady. When the wind speed exceeds approximately 20 MPH or if there is no wind and/or the wind direction is too variable, dispersion patterns conducive to accurate sampling are disturbed and quantitative mass to mass relationships are difficult to establish. The upper limit of stress with respect to meteorological conditions can be examined by the spread of mass to mass ratios for each individual sample for a given sampling run. If the calculated ratios are inconsistent or the deviation between each calculated ratio and their mean is greater than 20%, it would be necessary to seek an explanation based on process variations or meteorological conditions or to void the sampling run and possibly suspend sampling until conditions are more favorable.

#### D-5 Field Sampling Strategy

The program for a sampling run will generally involve the collection of triplicate downwind samples and a single point upwind sample. Actual sampler locations will be determined by the gas chromatograph on



site. Grab samples will be collected in glass flasks and analyzed to determine the benzene concentration in the vicinity of the source to be tested. This information will be correlated with wind speed and direction to choose the exact sampler locations. In the ideal case downwind samplers will be equidistant from the source and along approximately a  $30^{\circ}$  arc.

Two sets of samples will be integrated over separate one-half hour periods and together constitute a single test. Samples will be collected by Environmental Measurements AQS II sampling system into clean 10-liter Tedlar bags. Tedlar bags to be reused for sampling will be flushed three times with nitrogen and allowed to sit overnight three quarters full. Prior to their next use each will be analyzed for benzene content.

The tracer gas dispersion apparatus will be positioned over the source to be tested as near as possible to the actual emissions. Ideally the dispersion tube or support member will span the source of the emissions at its center.



TABLE D-1

## EXPERIMENTAL DATA

Release Rate g/min	Benzene Release Method	Sample Type	Wind Speed	Wind Direction	Theoretical T <sub>0</sub> /ic <sub>4</sub>	$\phi$ /ic <sub>4</sub> #1	$\phi$ /ic <sub>4</sub> #2	$\phi$ /ic <sub>4</sub> #3	Average
$\phi$ 0.027 ic <sub>4</sub> 5.26	Evaporation	Grab	0-5 MPH	Steady	0.005	*NO	NO	NO	---
$\phi$ 0.993 ic <sub>4</sub> 8.27	Evaporation	Grab	0-5 MPH	Steady	0.120	*NO	NO	NO	---
$\phi$ 4.05 ic <sub>4</sub> 7.16	Evaporation	Grab	0-5 MPH	Steady	0.59	0.64	0.64	0.65	0.645
$\phi$ 9.40 ic <sub>4</sub> 6.38	Evaporation	Integrated	5-10 MPH	Steady	1.47	1.57	1.43	---	1.50
$\phi$ 10.85 ic <sub>4</sub> 13.59	Evaporation	Integrated	20-25 MPH	Variable	0.80	1.29	1.82	0.94	1.35
$\phi$ 9.40 ic <sub>4</sub> 8.25	Bubbler	Integrated	15-20 MPH	Steady	1.14	1.40	1.93	1.02	1.18
$\phi$ 6.33 ic <sub>4</sub> 6.48	Bubbler	Integrated	0-5 MPH	Steady	0.91	0.97	0.96	0.96	0.96
$\phi$ 6.48 ic <sub>4</sub> 6.48	Bubbler	Integrated	0-5 MPH	Steady	1.00	0.91	0.86	0.89	0.89

 $\phi$  - Benzeneic<sub>4</sub> - Isobutane

\* No benzene, only Isobutane detected.





**APPENDIX E**  
**PROJECT PARTICIPANTS**



**Scott Environmental Technology Inc.**

APPENDIX E

PROJECT PARTICIPANTS

The following people participated in some phase of the sampling program at Republic Steel, Gadsden, Alabama.

From Scott Environmental Technology, Inc.:

Tom Bernstiel, Chemist

Jack Carney, Chemist

P. K. Chattopadhyay, Chemist

Dan FitzGerald, Manager, Eastern Operations

Kevin Gordon, Technician

Carolyn Graham, Chemical Engineer

Lou Reckner, Vice President & General Manager

From Research Triangle Institute:

Peter Mehta

From U. S. Environmental Protection Agency

Dan Bivins



UNITED STATES ENVIRONMENTAL PROTECTION AGENCY

Office of Air Quality Planning and Standards  
Research Triangle Park, North Carolina 27711

DATE: 4/21/81

SUBJECT: Source Test Report

FROM: J. E. McCarley, Chief, Field Testing Section,  
Emission Measurement Branch, ESED (MD-13)

TO: See Below

The enclosed final source test report is submitted for your information. Any questions regarding the test should be directed to the Project Officer (telephone: 8/629-5543). Additional copies of this report are available from the ERC Library, Research Triangle Park, North Carolina 27711.

Industry: Benzene

Process: Coke Oven By-Product

Company: Republic Steel Corporation

Location: Gadsden, Alabama

Project Report Number: 80-BYC-4

Project Officer: Dan Bivins

Enclosure

Addressees:

Ken Knapp, ESRL (MD-46)

Arch MacQueen, MDAD (MD-14)

Rodney Midgett, EMSL (MD-77)

Mark S. Siegler, DSSE (MD-EN-341)

Director, Air & Hazardous Materials Division, Region IV

(copy enclosed for State agency)

Bob Kilgore, EPA Library Services (MD-35)