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AP-42 Section	<u>12.2</u>
Reference	<u> </u>
Report Sect.	<u>4</u>
Reference	<u>44</u>

PARTICULATE EMISSIONS EVALUATION

"A" BATTERY SCRUBBER STACK

Reviewed

AT

BETHLEHEM STEEL CORPORATION
BETHLEHEM, PENNSYLVANIA 18061

BCM NO. 00-4021-37

DECEMBER 10, 1992

PREPARED BY

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File

COMMONWEALTH OF PENNSYLVANIA

DATE:

December 30, 1992

SUBJECT: "A" BATTERY SCRUBBER STACK TEST

Bethlehem Coke Works
Bethlehem Steel Corp.
Bethlehem, Northampton County

TO:

L. Blaine DeHaven
Source Testing & Monitoring Section

THRU: Thomas A. DiLazaro
Acting Air Quality
Program Manager

FROM:

Ronald D. Mordosky *RDM*
Air Quality Specialist

Please review the attached stack test to determine if the procedures used comply with the Department's regulations.

RDM/bas

Attachment

DEC 31 1992

2/26

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1.0 EXECUTIVE SUMMARY

Bethlehem Steel Corporation retained BCM Engineers Inc. (BCM) to perform a particulate emissions test on the "A" Coke Battery Pushing Scrubber Exhaust Stack located in Bethlehem, Pennsylvania. Testing and analyses were conducted in accordance with EPA Methods One through Five and Pennsylvania Department of Environmental Resources (PADER) methodology. The test results are to be used to demonstrate compliance with limitations set forth by PADER. The measured particulate emission was 0.76 lb/hr. The compliance limit was 4.71 lb/hr.

2.0 SCOPE AND OBJECTIVES

The scope of this project was outlined in BCM Proposal No. 13-8590-01. The following parameters were determined for the test run:

- | | |
|-------------------------|-------------------|
| • Gas Flow | acfm and dscfm |
| • Gas Temperature | °F |
| • Gas Moisture | % by Volume |
| • Particulate Emissions | gr/dscf and lb/hr |

3.0 PROCEDURES

The field sampling program was performed on November 24, 1992. The BCM test personnel consisted of Messrs. Paul Jadlovec, Nick Charno, and Karl Brenton. Mr. Lawrence Kreiger served as plant coordinator.

3.1 FIELD WORK

3.1.1 Field Data Sheets

All field data sheets are contained in Appendix A.

3.1.2 Testing Station and Traverse Locations

The exhaust stack has an internal diameter of 96 inches at the test location. The test elevation is located approximately 50 feet or 6 stack diameters downstream from the inlet breeching and approximately 16 feet or 2 stack diameters upstream from the stack outlet. EPA Method One was utilized to determine the number and location of the traverse points. Sixteen (16) points were sampled, 4 at each of 4 sample ports located 90 degrees to center.

3.1.3 Gas Flow and Gas Temperature Measurements

The flow rate and temperature profiles for the gas streams were measured by conducting simultaneous velocity and temperature traverses. Gas velocity head was measured with a calibrated "S"-type Pitot tube which was connected to an inclined manometer. The static pressure was measured using the same Pitot tube and manometer. A Chrome-Alumel thermocouple attached to a digital potentiometer was used to measure the gas temperature at each of the traverse points. The gas flow and gas temperature measurements followed EPA Method Two.

3.1.4 Molecular Weight Determination

A Bacharach Fyrite analyzer was used to determine the molecular weight of the flue gas. Fyrite gas analyzers give accurate readings within +/- 0.5% Carbon Dioxide or Oxygen up to 538°C. Readings are unaffected by most other gases. The following parameters were measured in order to calculate molecular weight: volume percent carbon dioxide and volume percent oxygen; the volume percent of carbon monoxide and nitrogen was determined by difference. These parameters were measured using the principle of gas absorption in specific absorbing solutions.

3.1.5 Moisture Content Sampling

Moisture sampling was conducted employing the principles presented in EPA Method Four and concurrently with particulate sampling. Parameters evaluated in order to determine the gas stream moisture content were: sample gas volume, sample gas temperature, sample gas pressure, impinger moisture gain, and silica gel moisture gain. Some minor modifications were made to the Method Four train to allow concurrent particulate and moisture content sampling; these modifications involve no deviations from sampling principles. Modifications such as the substitution of a glass fiber filter for Pyrex wool as a filtering medium and the substitution of a calibrated orifice for a rotameter as a flow metering device were incorporated.

3.1.6 Determination of Particulate Emissions

Sampling procedures followed those described in EPA Method Five and PADER Bureau of Air Quality Control, Division of Technical Services and Monitoring, "Source Testing Manual." A schematic of the sampling train is presented in Figure 1.

3.1.7 Sample Recovery Procedure

Sample recovery was conducted onsite in the BCM test van.

3.1.8 Operational Data

The coke production rate of 1,850 tons/day for "A" Coke Battery was provided by Bethlehem Steel.

3.2 ANALYSIS

All analytical data sheets are contained in Appendix B. All sample analyses were conducted by BCM at their Pittsburgh office.

3.3 CALCULATIONS

The BCM Computation Sheets contained in Appendix C show the coke production rate and allowable and actual emission rate calculations. The coke production rate of 77.08 tons per hour was calculated using the production value of 1850 tons of coke per day and 80 ovens pushed in 24 hours. The allowable emission rate was calculated according to 123.13(b)(2) of the Pennsylvania Air Pollution Control Act. The actual particulate emission rate was calculated from the particulate concentration (gr/dscf), the stack gas flow rate (dscf/min), and the coke pushing time (min/hr). The coke push time was calculated from the average duration of a single push determined during the test run and the historical number of ovens pushed in 24 hours.

Particulate emission calculations were completed using a Lotus 123 spreadsheet format. The results of each pertinent parameter are detailed on the spreadsheet. The averages for the sampling data were time weighted.

3.4 CALIBRATIONS

The following field equipment calibrations are contained in Appendix D:

- Dry Gas Meter and Orifice
- Thermocouple
- Pitot Tube
- Nozzle Diameter

4.0 SUMMARY OF RESULTS

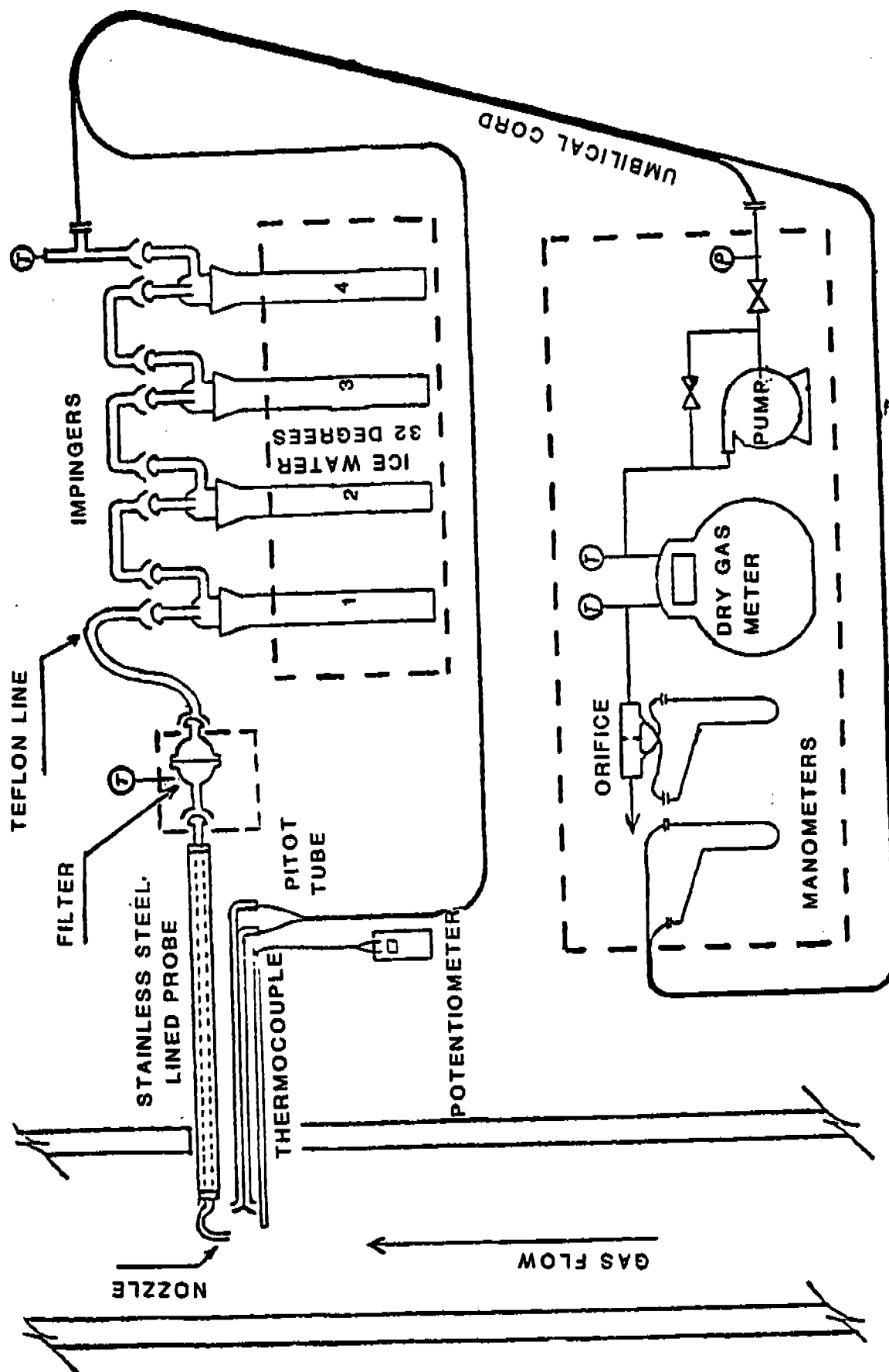
A summary of the test results are contained in Table 1. All data were collected during the 16 separate oven pushes. Values as presented in Table 1, therefore, represent stack conditions during pushing operations. The particulate emission rate, however, was calculated to represent the actual pounds of particulate emitted in an hour period, based on the minutes per hour of pushing time.

The actual emission rate measured was 0.76 lb/hr. The allowable emission rate was 4.71 lb/hr.

TABLE 1
SUMMARY OF RESULTS
"A" BATTERY SCRUBBER STACK

Parameter	Results
Gas Flow (acfm)	143,812
Gas Flow (dscfm)	133,760
Gas Temperature (^o F)	93.9
Gas Moisture (%)	0.6
Isokinetic (%)	99.5
Actual Particulate Emissions: gr/dscf	0.00900
lb/hr	0.76
Allowable Particulate Emissions: lb/hr	4.71
Backhalf Soluble Emissions: gr/dscf	0.00111

FIGURE 1



METHOD 5 SCHEMATIC

APPENDIX A
FIELD DATA SHEETS

BCM

PLANT

DATE 11-24-92

RUN NUMBER

BATTERY A SCRUBBER OUTLET RUN 1

[illegible]

APPENDIX B
ANALYTICAL DATA SHEETS

BLANK ANALYTICAL DATA

Plant BETHLEHEM STEEL

Sample location "A" BATTERY STACK

Type of blank ACETONE

Container number 16W

Density of blank (ρ_a) .7850 g/ml

Blank volume (V_a) 150 ml

Gross wt. 112148.65 mg

Tare wt. 112148.60 mg

Weight of blank (m_a) .05 mg

$$C_a = \frac{m_a}{V_a \rho_a} = \frac{(.05)}{(150) (.7850)} = .0004 \text{ mg/g}$$

BLANK ANALYTICAL DATA

Plant BETHLEHEM STEEL

Sample location "A" BATTERY STACK

Type of blank WATER

Container number 17C

Density of blank (ρ_a) .9982 g/ml

Blank volume (V_a) 150 ml

Gross wt. 108457.40 mg

Tare wt. 108459.75 mg

Weight of blank (m_a) 0.00 mg

$$C_a = \frac{m_a}{V_a \rho_a} = \frac{(0.00)}{(150)(.9982)} = 0.00 \text{ mg/g}$$

ANALYTICAL PARTICULATE DATA

PADER METHODOLOGY

Client BETHLEHEM STEEL Project No. 00-4021-37
Sample location "A" BATTERY STACK
Date 11-24-92 Run No. 1

SOLUBLE BACKHALF

Acetone rinse container No. 16Y
Acetone rinse volume (Vaw) 77
Acetone blank residue concentration (Ca) .0004 mg/g
 $Wa = Ca Vaw pa = (.0004) (77) (.9982) = .024$ mg
Gross wt 102291.25 mg
Tare wt 102289.85 mg
Less acetone blank wt (Wa) .024 mg
Weight of particulate in acetone rinse 1.38 mg

Water filtrate container No. 16L
Water filtrate volume (Vww) 227
Water blank residue concentration (Cw) 0.00 mg/g
 $Ww = Ca Vww pa = (0.00) (227) (.9982) = 0.00$ mg
Gross wt 112012.10 mg
Tare wt 112013.70 mg
Less water blank wt (Ww) 0.00 mg
Weight of particulate in water filtrate 0.00 mg
Weight of particulate in acetone rinse 1.38 mg
Total weight of particulate 1.38 mg

APPENDIX C
CALCULATIONS

ANALYTICAL PARTICULATE DATA

PADER METHODOLOGY

Client BETHLEHEM STEELProject No. 00-4021-37Date 11-24-92Run No. 1

FRONT HALF CATCH

Acetone rinse container No. 16J
 Acetone rinse volume (Vaw) 88
 Acetone blank residue concentration (Ca) .0004 mg/g
 $W_a = Ca Vaw p_a = (.0004) (88) (.7850) = .028$
 Gross wt 113106.35 mg
 Tare wt 113100.20 mg
 Less acetone blank wt (W_a) .028 mg
 Weight of particulate in acetone rinse 6.122 mg

Water rinse container No. 16Z
 Water rinse volume (Vww) 84
 Water blank residue concentration (Cw) 0.0 mg/g
 $W_w = Ca Vww p_a = (0.0) (84) (.9982) = 0.0$
 Gross wt 99946.35 mg
 Tare wt 99942.60 mg
 Less water blank wt (W_w) 0.00 mg
 Weight of particulate in water rinse 3.75 mg

Filter No. 545
 Gross wt 410.75 mg
 Tare wt 409.05 mg
 Weight of particulate on filter 1.700 mg
 Weight of particulate in acetone rinse 6.122 mg
 Weight of particulate in water rinse 3.750 mg
 Total weight of particulate 11.572 mg

BACK HALF CATCH

Filter No. .45 506 .22 503
 Gross wt 167.90 mg
 Tare wt 168.45 mg
 Weight of particulate on filter 0.00 mg

TOTAL PARTICULATE CATCH

Front half 11.572 mg
 Back half 0.00 mg
 Total 11.572 mg

BETHLEHEM STEEL CORPORATION
BETHLEHEM PENNSYLVANIA
"A" BATTERY SCRUBBER EXHAUST

11-24-92
RUN 1

PARTICULATE EMISSIONS

SYMBOL	DESCRIPTION	VALUE
Theta	= Duration of test, min.	= 21.18
Vm	= Dry sample volume (meter conditions), dcf	= 19.185
SQRT(dP)	= Average of square roots of pitot pressure differential, in. H ₂ O	= 0.820
dH	= Orifice pressure drop, in. water	= 2.830
Ts	= Average stack temperature, deg. F	= 93.9
Tm	= Average dry gas meter temperature, deg. F	= 56.4
CO ₂	= CO ₂ in stack gas, %	= 0.00
O ₂	= O ₂ in stack gas, %	= 20.90
CO	= CO in stack gas, %	= 0.00
N ₂	= N ₂ in stack gas, %	= 79.10
Pbar	= Barometric pressure, in. Hg	= 29.35
Ps	= Stack pressure (absolute), in. Hg.	= 29.37
Cp	= Pitot correction factor, dimensionless	= 0.84
Y	= Dry gas meter correction factor	= 0.987
Dn	= Diameter of nozzle, in.	= 0.250
Ds	= Diameter of stack, ft.	= 8.000
Vlc	= Volume of liquid collected in impingers and silica gel, ml	= 2.3
Mn	= Front half particulate catch, mg	= 11.57
Mn	= Back half insoluble part. catch, mg	= 0.00
Mn	= Back half soluble part. catch, mg	= 1.38
Mn	= Total particulate catch, mg	= 11.57
An	= Area of the nozzle, sq. ft.	= 0.00034
As	= Area of the stack, sq.ft.	= 50.27
Md	= Dry molecular weight of stack gas, dry basis, lb/lb-mole	= 28.84
Vw(std)	= Volume of liquid collected, cu .ft.	= 0.108
Ms	= Molecular weight of stack gas, wet basis, lb/lb-mole	= 28.77
Vm(std)	= Dry sample volume (standard conditions), dscf	= 19.119
Vs	= Stack velocity, ft/sec	= 47.68

BETHLEHEM STEEL CORPORATION
 BETHLEHEM PENNSYLVANIA
 "A" BATTERY SCRUBBER EXHAUST

11-24-92
 RUN 1

PARTICULATE EMISSIONS

SYMBOL	DESCRIPTION	VALUE
Qs	= Stack gas flow, acfm	= 143812
Qsd	= Stack gas flow, dscfm	= 133760
Bws	= Moisture content of the gas stream, %	= 0.6
CO2	= CO2 in stack gas, %	= 0.00
O2	= O2 in stack gas, %	= 20.90
CO	= CO in stack gas, %	= 0.00
N2	= N2 in stack gas, %	= 79.10
I	= Isokinetic ratio, percent	= 99.5
C's	= Particulate concentration, gr/dscf	= 0.00900

PADER INFORMATION

C's	= Part. conc. (front half), gr/dscf	= 0.00900
C's	= Part. conc. (back half), gr/dscf	= 0.00000
C's	= Part. conc. soluble, (back half), gr/dscf	= 0.00111



COMPUTATION SHEET

Name of Client Bethlehem Steel Corporation
Project "A" Battery Scrubber Stack
Description Emission Rate Calculation

Sheet Number	<u>1</u>	of	<u>2</u>
Date	<u>11-8-92</u>		
Job Number	<u>00-4021-37</u>		
Computed by	<u>PJ</u>	Checked by	

Coke Production Rate

1850 Tons/Day and 80 ovens Pushed/Day

$$\therefore \frac{1850 \text{ Tons/Day}}{80 \text{ ovens/Day}} = 23.12 \text{ Tons/oven}$$

$$23.12 \text{ Tons/oven} \times 80 \text{ ovens/24 hours} = 77.07 \text{ Tons/hour}$$

Allowable Emission Rate, as per 123.13 (b)(2) of PA Air Pollution Control Act

$$A = 0.76 E^{0.42}$$

where: A = allowable emission rate, lb/hr
 E = $F \times W$, lb/hr
 F = Process Factor (table 1), 1 lb/ton
 W = Production Rate, 77.07 Tons/hour

$$A = 0.76 (1 \text{ lb/ton} \times 77.07 \text{ Tons/hr})^{0.42} = \underline{\underline{4.71 \text{ lb/hr}}}$$



COMPUTATION SHEET

Name of Client Bethlehem Steel CorporationProject "A" Battery Scrubber StackDescription Emission Rate CalculationSheet Number 2 of 2Date 11-8-92Job Number 00-4021-37Computed by PJ Checked by

$$\text{Actual Emission Rate (lb/hr)} = \frac{\left(\text{Emission Concentration (gr/dscf)} \right) \left(\text{Flow Rate (dscf/min)} \right) \left(\text{Push Time (min/hr)} \right)}{7000 \text{ gr/lb}}$$

where:

$$\begin{aligned} \text{Emission Concentration} &= \text{gr/dscf} \\ \text{Flow Rate} &= \text{dscf/min} \end{aligned}$$

$$\begin{aligned} \text{Push Time} &= \left(\frac{2.18 \text{ min total push time}}{16 \text{ Total Ovens Pushed}} \right) \left(\frac{80 \text{ ovens pushed}}{24 \text{ hours}} \right) \\ &= 4.41 \text{ min/hr} \end{aligned}$$

$$\begin{aligned} \text{Actual Emission Rate (lb/hr)} &= \frac{(0.009 \text{ gr/dscf}) (133.760 \text{ dscf/min}) (4.41 \text{ min/hr})}{7000 \text{ grains/lb}} \\ &= \underline{\underline{0.76 \text{ lb/hr}}} \end{aligned}$$

APPENDIX D
CALIBRATIONS

BCM

METER BOX CALIBRATION SHEET

Date 11-11-92 Box No. A-1 Inspector J. STETINA

Pump OK oil ANNIE Wick CF#1 Drum Serial No.

Manometers OK Lo&D, Knobs OK Oil OK Tubing OK

Quick Connects OK Vacuum Gauge OK Valves OK

Dry Gas Meter OK Volume 485 ft³ Serial No.

Thermometers In 74 of Out 74 of Ambient 74 of

Amphenol OK Lights OK Switches OK Variac OK

Leak Check - Max. Vacuum 26 in. Hg Leak Rate 0.04 CFM

Remarks changed resistor connection & pyrometer

2.70 dead out 29.70

Man. Orifice	CF _w	CF _d	T _w	IT _d	OT _d	T _d	Time θ
0.5	6.506	6.813	73	104	84	94	15:40 15:57
1.0	6.500	6.782	73	100	80	90	11:54 11:59
2.0	10.006	10.610	73	117	87	102	13:15 13:25

Tolerances: $1.6 \leq \Delta H_{\theta} \leq 2.1$

$\Delta H_{\theta} =$	$\frac{(0.0317)(\Delta H)}{(P_b)(OT_d + 460)} \left[\frac{(T_w + 460)(\theta)^2}{(CF_w)} \right]$	$\gamma =$	$\frac{(CF_w)(P_b)(T_d + 460)}{(CF_d)(P_b + \Delta H/13.6)(T_w + 460)}$
1.62	$\frac{(0.0317)(0.5)}{(21.72)(84 + 460)} \left[\frac{(73 + 460)(15.67)^2}{(6.506)} \right]$	991	$\frac{(6.506)(21.7)(94 + 460)}{(6.813)(22.7 + 0.0368)(73 + 460)}$
1.88	$\frac{(0.0317)(1.0)}{(21.7)(80 + 460)} \left[\frac{(73 + 460)(11.9)^2}{(6.5)} \right]$	987	$\frac{(6.5)(21.7)(90 + 460)}{(6.782)(22.7 + 0.0737)(73 + 460)}$
1.94	$\frac{(0.0317)(2.0)}{(21.7)(87 + 460)} \left[\frac{(73 + 460)(13.25)^2}{(10.006)} \right]$	989	$\frac{(10.610)(21.7)(102 + 460)}{(10.610)(21.7 + 0.147)(73 + 460)}$

CONSTRUCTION STANDARDS:

1. $D_t =$ between .187" - .375" (3/16 - 3/8)
2. $P_A = P_B$; $1.05 \cdot D_t \leq P \leq 1.50 \cdot D_t$
3. $a_1 \cdot a_2 < 10^\circ$
4. $B_1 \cdot B_2 < 5^\circ$
5. $Z \leq 0.125"$ (1/8)
6. $W \leq 0.031"$ (1/32)

PITOT ALIGNMENT STANDARDS:

1. $x \geq 0.75"$ (3/4)
2. l_p must be higher than N_p
3. $W \geq 3.0"$
4. $Z \geq 0.75"$ (3/4)
5. $Z_1 \geq 2.0"$
6. $Y \geq 3.0"$

TYPE S PITOT
CALIBRATION STANDARDS



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ENGINEERS, PLANNERS, SCIENTISTS
and LABORATORY SERVICES

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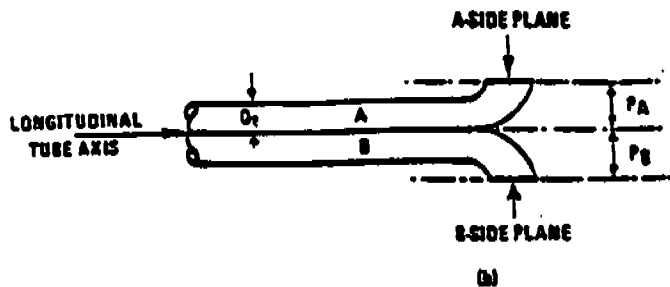
DATE: 4-17-92

PITOT I.D.: 4-2

REF. NO.: 5-10

PAGE NO.: 1 of 4

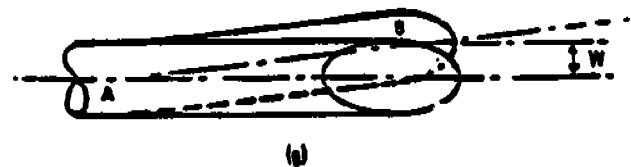
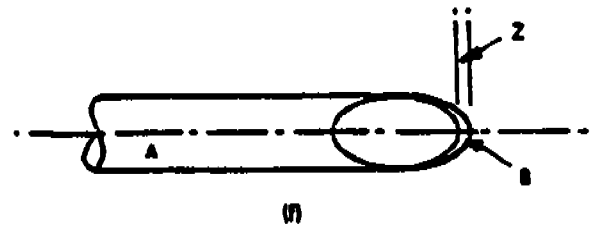
PITOT CONSTRUCTION CALIBRATIONS



$D_t =$.375

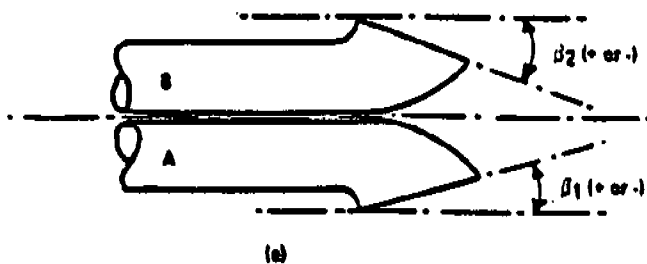
$P_A =$.46

$P_B =$.46



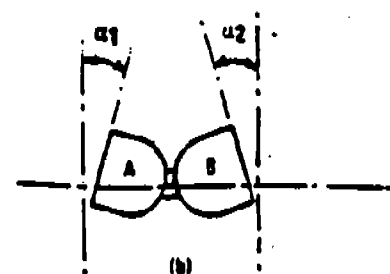
$Z =$ 0

$W =$ 0



$B1 =$ 0°

$B2 =$ 2°



$a1 =$ 8°

$a2 =$ 4°

Performed by JS

TYPE S PITOT
CALIBRATION STANDARDS



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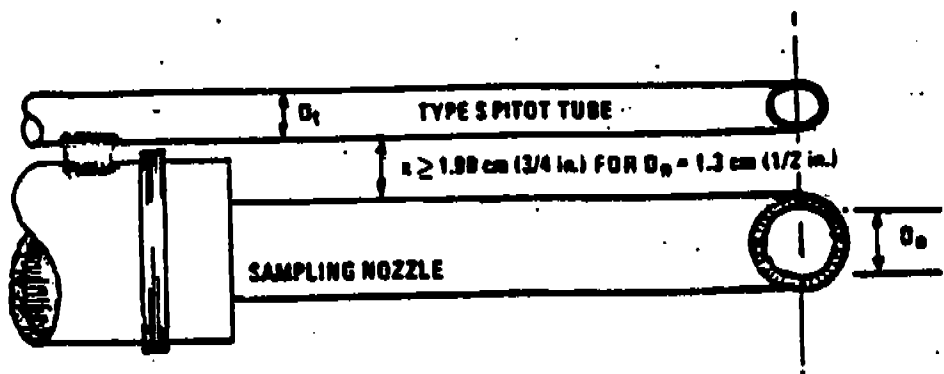
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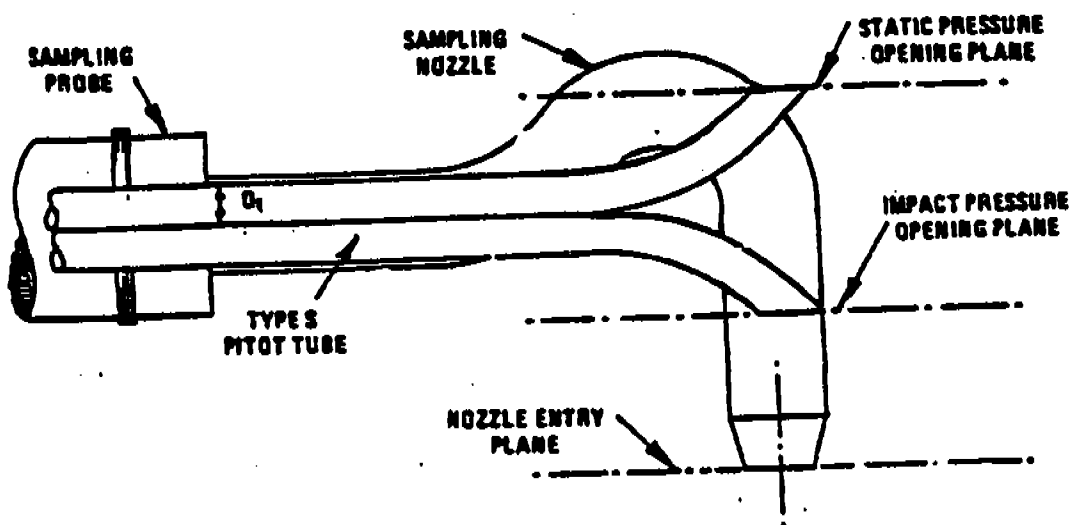
REF. NO.: S-10

PAGE NO.: 2 of 4

PITOT ALIGNMENT/NOZZLE CALIBRATIONS



X = .85



Is IP higher than NP? YES

Performed By J.S.

TYPE S PITOT TUBE
CALIBRATION STANDARDS



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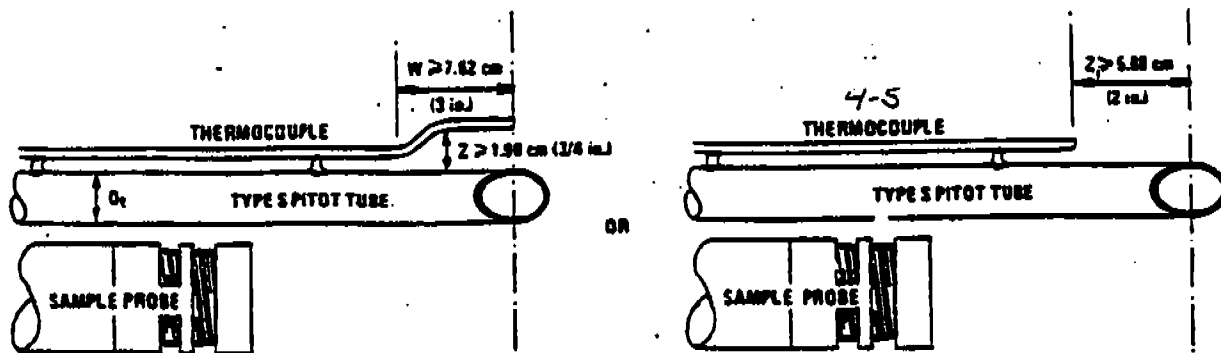
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REF. NO.: 5-10

PAGE NO.: 3 of 4

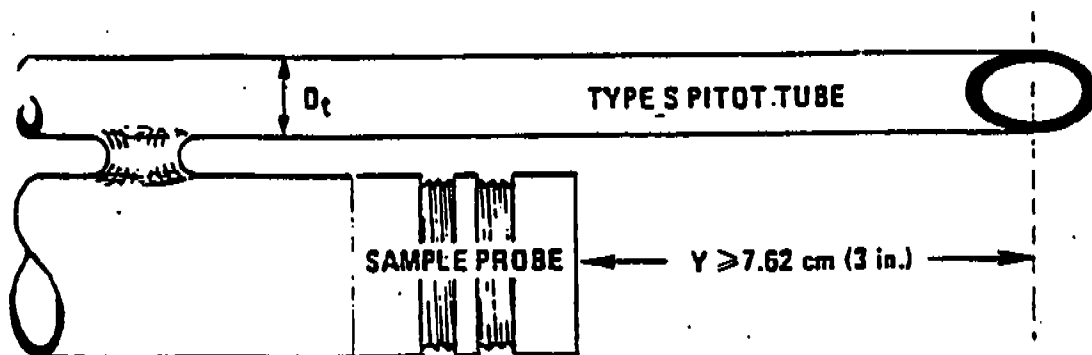
PITOT ALIGNMENT/THERMOCOUPLE CALIBRATION



W = _____

$Z_1 = \underline{\quad 2 \quad}$

$Z' = \underline{\hspace{2cm}}$



Y = 3

Determined Coefficient .84

Performed by JS

**TYPE S PITOT TUBE
CALIBRATION STANDARDS**



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DATE: 4-17-92

PITOT I.D.: 4-2

REF. NO.: 5-10

PAGE NO.: 4 of 4

PYROMETER CALIBRATION SHEET

Pyrometer Meterbox A-1

Date 11-13-72

Inspector J. STETINA

<u>Indicated Temperature (From pyrometer)</u>	<u>Actual Temperature (From standard)</u>	<u>Difference</u>
100	<u>99</u>	<u>1</u>
200	<u>200</u>	<u>0</u>
300	<u>299</u>	<u>1</u>
400	<u>397</u>	<u>3</u>
500	<u>498</u>	<u>2</u>
600	<u>600</u>	<u>0</u>
700	<u>699</u>	<u>1</u>
800	<u>801</u>	<u>1</u>
900	<u>899</u>	<u>1</u>
1000	<u>1000</u>	<u>0</u>
1100	<u>1099</u>	<u>1</u>
1200	<u>1198</u>	<u>2</u>
1300	<u>1299</u>	<u>1</u>
1400	<u>1400</u>	<u>0</u>
1500	<u>1500</u>	<u>0</u>
1600	<u>1600</u>	<u>0</u>
1700	<u>1699</u>	<u>1</u>
1800	<u>1800</u>	<u>0</u>
1900	<u>1899</u>	<u>1</u>
2000	<u>2000</u>	<u>0</u>
Avg.		<u>...</u>

NOZZLE CALIBRATION

Date 11-24-42

Calibrated by Paul Jablowiec

Nozzle identification number	D_1 , in.	D_2 , in.	D_3 , in.	ΔD , in.	D_{avg}
Bath. Size 1 A Battery Screener Stack Test	.250	.250	.250	.000	.250

where:

$D_{1,2,3}$ = nozzle diameter measured on a different diameter, in.
Tolerance = measure within 0.001 in.

ΔD = maximum difference in any two measurements, in.
Tolerance = 0.004 in.

D_{avg} = average of D_1 , D_2 , and D_3 .

Nozzle calibration data.

