



Air Quality Test Report

EPA Compliance Testing for Particulate Matter and
Volatile Organic Compound Emissions

EAF #1 (SN-01)

EAF #2 (SN-12)

Quanex Corp. - MacSteel Division
Ft. Smith, Arkansas

April 17 - 20, 2007

ADEQ Permit # 693-AOP-R4; 66-0274

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INTRODUCTION

MacSteel located in Ft. Smith, Arkansas is operating a steel mill facility in the production of various steel products. As part of the air quality control system, two positive pressure baghouses are operated to limit the air pollution emissions from the electric arc furnace (EAF) utilized in the scrap melting process. The facility performed emissions testing to demonstrate air quality compliance established in the operating permit (#693-AOP-R4). Sampling and analysis was performed for particulate matter, (PM), total hydrocarbons (excluding methane), and volumetric flow rate.

The particulate matter determination was performed utilizing EPA Reference Methods 5 and 5D for SN-01 and SN-12 respectively. The test result values are provided in grains per dry standard cubic foot (gr/dscf) and pounds per hour (lb/hr). These samples were collected over three 4-hour periods.

Volatile organic compound (VOC) emissions were determined from each EAF exhaust. The results for the VOC's were obtained over three (3) sixty minute periods simultaneously from each source. The pollutant values are provided in parts per million (ppm) and pounds per hour (lb/hr). Additionally, methane analysis was performed on each point source to provide a total non-methane hydrocarbon result. Samples were gathered during each VOC run using tedlar bags to obtain an integrated sample. The emissions determination was performed according to EPA Reference Methods 25A. The testing procedures were performed on April 17-20, 2007.

SUMMARY OF RESULTS

Particulate Matter (PM)

EAF # 1 (SN-01)			
Date/Time	Isokinetics	gr/dscf	lb/hr
4/19;08:40-13:05	105.49	0.00046	1.50
4/19;13:50-18:05	106.52	0.00041	1.45
4/20;08:25-12:40	104.39	0.00048	1.69
Average:	105.47	0.00045	1.55
EAF # 2 (SN-12)			
Date/Time	Isokinetics	gr/dscf	lb/hr
4/17;09:05-13:20	106.53	0.0003	1.84
4/17;14:20-18:35	103.72	0.0005	3.29
4/18;09:30-13:45	101.16	0.0003	1.76
Average:	103.8	0.0004	2.30
PM Compliance Summary			
Test	CST*, gr/dscf		lb/hr
1	0.00035		3.34
2	0.00047		4.74
3	0.00036		3.45
Average	0.00039		3.84
Limit	0.0018		27.4

Based upon the emission results, the processes designated as SN-01 and SN-12 are operating within the allowable limit for particulate matter emissions.

SUMMARY OF RESULTS

Total Non-Methane Hydrocarbon Compounds (TNMHC)
Emissions Summary
April 17-20, 2007

EAF # 1 (SN-01)				
Run	Time	TNMHC, ppm (THC-CH ₄)	Vol. Flow (SCFM)	Emission (lb/hr)
1	11:30-12:30	(7.6-7.4) = 0.2	383,798	0.19
2	14:30-15:30	(7.8-7.2) = 0.6	415,235	0.62
3	09:15-10:15	(9.7-9.6) = 0.1	408,634	0.10
Average	-	0.3	402,556	0.30
EAF # 2 (SN-12)				
Run	Time	TNMHC, ppm (THC-CH ₄)	Vol. Flow (SCFM)	Emission (lb/hr)
1	09:05-10:05	(12.2-12.0) = 0.0	789,044	0.00
2	14:00-15:00	(9.8-9.4) = 0.4	761,383	0.76
3	09:30-10:30	(10.7-10.6) = 0.1	763,273	0.19
Average	-	0.2	771,233	0.32
Combined lb/hr:				0.62
Limit:				11.2

Based upon the emission results, the processes designated as SN-01 and SN-12 are operating within the allowable emission rates for total hydrocarbons emissions.

CALCULATIONS

The following section provides a detailed description of all calculations used in the determination of emission rates. Also listed are all of the intermediate values associated with these calculations.

EAF #1 (SN-01)

Dry Gas Meter Volume

$$V_{m(std)} = V_m \left[\frac{T_{STD}}{T_m} \right] \left[\frac{P_{bar} + \frac{\Delta H}{13.6}}{P_{std}} \right] = 17.64[Y] \left[V_m \right] \left[\frac{P_{bar} + \frac{\Delta H}{13.6}}{T_m} \right]$$

Parameter	Run 1	Run 2	Run 3
V _m	165.925	180.832	175.087
T _m	517	516	518
P _{bar}	29.98	29.98	29.98
ΔH avg	1.56	1.79	1.74
C Factor (Y)	1.012	1.012	1.012
V _{m std}	172.589	188.563	181.845

Nomenclature

- ΔH = Average pressure drop across orifice, in. H₂O.
 P_{bar} = Barometric pressure, in. Hg.
 T_m = Absolute gas meter temperature, °R
 V_m = Dry gas volume measured, ft³
 Y = Dry gas meter calibration factor
 V_{m(std)} = Dry gas volume corrected to dry, standard conditions, ft³

Water Vapor Condensed

Moisture Content

Parameter	Run 1	Run 2	Run 3
V_{wc}	0.235	0.235	0.235
V_{wsg}	1.415	1.650	0.943
Bws, %	0.95	0.99	0.64

Nomenclature:

- B_{ws} = Water vapor, by volume, in gas stream, %
- ΔH = Average pressure drop across orifice, in. H_2O .
- P_{bar} = Barometric pressure, in. Hg.
- T_m = Absolute gas meter temperature, °R
- V_f, V_i = Impinger system volume, final & initial, ml
- V_m = Dry gas volume measured, ft^3
- $V_{m(std)}$ = Dry gas volume corrected to dry, standard conditions, ft^3
- $V_{wc(std)}$ = Water vapor condensed, ml
- $V_{wsg(std)}$ = Water vapor captured in silica gel, g
- W_f, W_i = Silica gel weight, final & initial, g
- Y = Dry gas meter calibration factor
- 0.04707 = Conversion factor, ft^3/ml
- 0.04715 = Conversion factor, ft^3/g

Dry Molecular Weight

$$M_d = 0.44[\%CO_2] + 0.32[\%O_2] + 0.28[\%CO + \%N_2]$$

Molecular Weight of Gas Stream

Parameter	Run 1	Run 2	Run 3
O ₂ , %	20.0	20	20
CO ₂ , %	0.5	0.5	0.5
CO + N ₂ , %	79.5	79.5	79.5
B _{ws} , %	0.95	0.99	0.64
M _d , lb/lb-mole	28.88	28.88	28.88
M _s , lb/lb-mole	28.78	28.77	28.81

Nomenclature

- B_{ws} = Water vapor, by volume, in gas stream, %
M_d = Dry molecular weight of gas stream, lb/lb-mole
M_s = Molecular weight of gas stream actual conditions, (lb/lb-mole)
%CO₂ = Carbon dioxide concentration, by volume, %
%O₂ = Oxygen concentration, by volume, %
%N₂ = Nitrogen concentration, by volume, %
%CO = Carbon monoxide concentration, by volume, %
18 = Molecular weight of H₂O vapor, lb/lb-mole

Linear Velocity of Gas Stream

Parameter	Run 1	Run 2	Run 3
K _p	85.49	85.49	85.49
C _p	0.84	0.84	0.84
SQRT (dP) avg	0.67	0.72	0.71
T _s , R	561	557	563
P _s	29.98	29.98	29.98
V _s	38.75	41.65	41.28

Volumetric Flow Rate of Gas Stream

Parameter	Run 1	Run 2	Run 3
B _{ws} , %	0.95	0.99	0.64
A _s , ft ²	176.71	176.71	176.71
T _s , R	561	557	563
P _s	29.98	29.98	29.98
Q _{sd} , SCFH	23,027,851	24,914,113	24,518,057

Nomenclature

- A = Cross sectional area of gas stream, ft²
 B_{ws} = Water vapor, by volume, in gas stream, %
 C_p = Calibration factor of pitot tube device, dimensionless
 ΔP = Pressure differential of gas stream, in H₂O
 K_p = 85.49 ft/sec[(lb/lb-mole•in. Hg)/(°K•in. H₂O)]^{1/2}
 M_s = Molecular weight of gas stream actual conditions, (lb/lb-mole)
 P_{bar} = Barometric pressure, in. Hg
 P_g = Static pressure of gas stream, in Hg
 P_s = Absolute pressure of gas stream, in. Hg (P_{bar}+P_g)
 P_{std} = Absolute standard pressure, 29.92 in. Hg
 Q_{sd} = Volumetric flow rate of gas stream, dry basis, std cond., ft³/hr
 T_s = Absolute temperature of gas stream, ° R
 T_{std} = Absolute standard temperature, 528° R
 V_s = Linear velocity of gas stream, ft/sec.
 3600 = Conversion factor, sec/hr.

Isokinetic Variation

$$I = 100 \cdot T_s \left[\frac{(0.002669) \left\{ V_{ic} + \left(\frac{Y_i \cdot V_m}{T_m} \right) \left(P_{bar} + \frac{\Delta H}{13.6} \right) \right\}}{60 \cdot V_s \cdot P_s \cdot A_n} \right]$$

Parameter	Run 1	Run 2	Run 3
Ts, R	561	557	563
Vic	35	40	25
Yi	1.012	1.012	1.012
Vm	165.925	180.832	175.087
Tm	517	516	518
Pbar	29.98	29.98	29.98
dH avg	1.56	1.79	1.74
sampling time, min.	240	240	240
An	0.000314	0.000314	0.000314
I	105.49	106.52	104.39

Nomenclature

- I = Isokinetic variation, %
- T_s = Absolute temperature of gas stream, ° R
- V_{ic} = Water vapor condensed from gas stream, ml
- Y = Dry gas meter calibration factor
- V_m = Dry gas volume measured, ft³
- T_m = Absolute gas meter temperature, °R
- P_{bar} = Barometric pressure, in. Hg.
- ΔH = Average pressure drop across orifice, in. H₂O.
- 13.6 = Inches of water per Hg.
- V_s = Linear velocity of gas stream, ft/sec.
- P_s = Absolute pressure of gas stream, in. Hg (P_{bar}+P_g)
- A_n = Cross sectional area of nozzle, ft²

Particulate Emission Rate Determination

$$C_s, \text{gr/dscf} = (0.0154 \text{ gr/mg})(m_n)/(V_{m \text{ std}})$$

$$E, \text{lb/hr} = (C_s)(Q_{sd})/(7000 \text{ gr/lb})$$

Particulate Matter & Lead

Parameter	Run 1	Run 2	Run 3
Particulate Matter			
m_n , mg	5.3	3.7	4.5
$V_{m \text{ std}}$, dscf	172.589	188.563	181.845
C_s , gr/dscf	0.00047	0.00030	0.00038
Q_{sd} , dscf/hr	23,027,851	24,914,113	24,518,057
E , lb/hr	1.56	1.08	1.33
Lead			
m_n , mg	0.0050	0.0050	0.0050
$V_{m \text{ std}}$, dscf	172.589	188.563	181.845
C_s , gr/dscf	4.46E-07	4.08E-07	4.23E-07
Q_{sd} , dscf/hr	23,027,851	24,914,113	24,518,057
E , lb/hr	0.0015	0.0015	0.0015

Nomenclature

m_n = Particulate matter collected, mg

$V_{m(\text{std})}$ = Dry gas volume corrected to dry, standard conditions, ft³

C = Concentration, grains per dry standard cubic foot (gr/dscf)

E = Pollutant emission rate, pounds per hour (lb/hr)

Q_{sd} = Gas stream volumetric flow rate, standard cubic feet per hour.

Gaseous Pollutant Emission Rate

$$E = (2.59 \times 10^{-9}) (MW) (ppm_d) (Q_{sd})$$

Run	TNMHC, ppm (THC-CH ₄)	Vol. Flow (SCFM)	Emission (lb/hr)
1	(7.6-7.4) = 0.2	383,798	0.19
2	(7.8-7.2) = 0.6	415,235	0.62
3	(9.7-9.6) = 0.1	408,634	0.10

Nomenclature

E = Pollutant emission rate, pounds per hour (lb/hr)

2.59×10^{-9} = Conversion factor

MW = Pollutant molecular weight, lb/lb-mole 16.04

ppm_d = Pollutant concentration, parts per million, dry basis

Q_{sd} = Gas stream volumetric flow rate, standard cubic feet per hour.

CALCULATIONS

The following section provides a detailed description of all calculations used in the determination of emission rates. Also listed are all of the intermediate values associated with these calculations.

EAF #2 (SN-12)

Dry Gas Meter Volume

$$V_{m(std)} = V_m \left[\frac{T_{std}}{T_m} \right] \left[\frac{P_{bar} + \frac{\Delta H}{13.6}}{P_{std}} \right] = 17.64[Y][V_m] \left[\frac{P_{bar} + \frac{\Delta H}{13.6}}{T_m} \right]$$

Parameter	Run 1	Run 2	Run 3
V _m	233.535	220.026	214.931
T _m	523	524	523
P _{bar}	30	30	30
ΔH avg	3.00	2.60	2.60
C Factor (Y)	0.997	0.997	0.997
V _{m std}	237.440	223.061	218.104

Nomenclature

- ΔH = Average pressure drop across orifice, in. H₂O.
- P_{bar} = Barometric pressure, in. Hg.
- T_m = Absolute gas meter temperature, °R
- V_m = Dry gas volume measured, ft³
- Y = Dry gas meter calibration factor
- V_{m(std)} = Dry gas volume corrected to dry, standard conditions, ft³

Linear Velocity of Gas Stream

$$V_s = \frac{Q_i * T_s * P_{std}}{A_s * 60 * T_{std} * (1 - B_{ws}) * P_s}$$

Parameter	Run 1	Run 2	Run 3
Inlet SCFM, Qi	789,087	761,383	763,273
T _s , R	692	578	584
B _{ws} , %	0.89	0.82	1.20
P _s	30	30	30
V _s	2.37	1.91	1.94

Nomenclature

A_s = Cross sectional area of measurement site, ft²
 Q_i = Volumetric flow rate of inlet gas stream, scfm
 B_{ws} = Moisture content, %
 P_s = Absolute pressure of gas stream, in. Hg ($P_{bar} + P_g$)
 T_s = Absolute temperature of gas stream at measurement site, ° R
 V_s = Linear velocity of gas stream at measurement site, ft/sec.

Isokinetic Variation

$$I = 100 \cdot T_s \left[\frac{(0.002669) \left\{ V_{ic} + \left(\frac{Y_i \cdot V_m}{T_m} \right) \left(P_{bar} + \frac{\Delta H}{13.6} \right) \right\}}{60 \cdot \pi \cdot V_s \cdot P_s \cdot A_n} \right]$$

Parameter	Run 1	Run 2	Run 3
Ts, R	692	578	584
Yi	0.997	0.997	0.997
Vm	233.535	220.026	214.931
Tm	523	524	523
Pbar	30	30	30
dH avg	3.00	2.60	2.60
sampling time, min.	240	240	240
An	0.0085221	0.0085221	0.0085221
I	106.53	103.72	101.16

Nomenclature

- I = Isokinetic variation, %
 T_s = Absolute temperature of gas stream, ° R
 V_{ic} = Water vapor condensed from gas stream, ml
 Y = Dry gas meter calibration factor
 V_m = Dry gas volume measured, ft³
 T_m = Absolute gas meter temperature, °R
 P_{bar} = Barometric pressure, in. Hg.
 ΔH = Average pressure drop across orifice, in. H₂O.
 13.6 = Inches of water per Hg.
 V_s = Linear velocity of gas stream, ft/sec.
 P_s = Absolute pressure of gas stream, in. Hg (P_{bar}+P_g)
 A_n = Cross sectional area of nozzle, ft²

Particulate Emission Rate Determination

$$C_s, \text{gr/dscf} = (0.0154 \text{ gr/mg})(m_n)/(V_{m \text{ std}})$$

$$E, \text{lb/hr} = (C_s)(Q_{sd})/(7000 \text{ gr/lb})$$

Parameter	Run 1	Run 2	Run 3
Particulate Matter			
m_n , mg	4.2	7.3	3.8
$V_{m \text{ std}}$, dscf	237.440	223.061	218.104
C_s , gr/dscf	0.0003	0.0005	0.0003
Q_{sd} , dscf/min	789,087	761,383	763,273
E , lb/hr	1.84	3.29	1.76
Lead			
m_n , mg	0.014	0.024	0.009
$V_{m \text{ std}}$, dscf	237.440	223.061	218.104
C_s , gr/dscf	9.08E-07	1.66E-06	6.35E-07
Q_{sd} , dscf/min	789,087	761,383	763,273
E , lb/hr	0.0061	0.0108	0.0042

Nomenclature

m_n = weight of particulate matter, mg

$V_{m(\text{std})}$ = Dry gas volume corrected to dry, standard conditions, ft³

C_s = Concentration of particulate matter, grains per dry standard cubic foot, gr/dscf

Q_{sd} = Volumetric flow rate of air being emitted, dry standard cubic feet per hour, dscf/hr

E = Pollutant emission rate, pounds per hour (lb/hr)

Gaseous Pollutant Emission Rate

$$E = (2.59 \times 10^{-9}) (MW) (ppm_d) (Q_{sd})$$

Run	TNMHC, ppm (THC-CH ₄)	Vol. Flow (SCFM)	Emission (lb/hr)
1	(12.2-12.0) = 0.0	789,044	0.00
2	(9.8-9.4) = 0.4	761,383	0.76
3	(10.7-10.6) = 0.1	763,273	0.19

Nomenclature

E = Pollutant emission rate, pounds per hour (lb/hr)

2.59×10^{-9} = Conversion factor

MW = Pollutant molecular weight, lb/lb-mole 16.04

ppm_d = Pollutant concentration, parts per million, dry basis

Q_{sd} = Gas stream volumetric flow rate, standard cubic feet per hour.

EQUIPMENT SPECIFICATIONS**Gaseous Analysis Equipment Specifications**

The following section provides a general description of each CEM analyzer utilized in the monitoring system. Detector type utilized, span values, etc. are provided.

**Reference Method Equipment
Component Listing**

Component	Manufacturer
THC Analyzer	J.U.M. Model VE-7
THC Analyzer	J.U.M. Model VE-7

Total Hydrocarbon Analyzer

A J.U.M. Model VE-7 was utilized to conduct the testing procedures for total hydrocarbons. This instrument performs continuous wet analysis of total hydrocarbons in gas mixtures.

The J.U.M. Model VE-7 is a highly accurate flame ionization detection (FID) gas analyzer. This analyzer utilizes a flame to combust the gas stream, which in turn enables detection through the ionization process. An internally mounted sample pump is used to draw sample gas through the detection system. The span value of the instrument was established as 100 ppm during the test procedures.

Heated Sample Line

The purpose of the Heated Sample Line is to transport the gas sample from the Probe Assembly to the analyzer system components. The HSL also maintains the gas sample temperature above the dew point to ensure moisture present in the gas stream does not condense out and interfere with proper system operation.

The HSL contains two teflon tubes within the outer shell and heat trace material. One of the tubes is used to transport the gas sample from the Probe Assembly to the analyzer system components. This tube is designated as the Sample Line. The second tube is utilized to transfer calibration gas to the probe for remote calibration purposes.

Data Acquisition System

Data Acquisition is performed by an Advantech analog to digital converter and utilizes Genie Data Acquisition Software to convert the voltage readings to meaningful concentration values.

EQUIPMENT SPECIFICATIONS

Particulate Analysis Equipment Specifications

Metering Console

An APEX Model 522 Metering Console was used to monitor the collection of the particulate samples, ensuring an isokinetic representation. The unit contains a dry gas meter with direct read index and a resolution of 0.001 cubic feet, separate temperature controllers for the heated probe and the particulate filter box, and thermocouple connections (type K) to monitor the temperature of the sample gas at critical sampling points throughout the sample train. Furthermore, the unit employs a dual-column, inclined/vertical manometer for determination of stack gas velocity and sample pump flow rate. The manometer has a range of 0 to 10 inches of water on both columns, with a resolution of 0.01 inches of water from the 0 to 1 inch range, and a resolution of 0.1 inches of water from the 0 to 10 inch range.

Sample Pump

An APEX Model E-0523 sample pump was used to draw a representative sample of the process exhaust gas stream across the sample filter. The flow rate of the Gast vane pump is controlled by the dual column manometer on the metering console along with a combination of needle valves. This allows the operator to draw the sample at an isokinetic rate corresponding to the stack gas flow rate.

Impinger Sample Train

The sample train used for the collection of particulate matter and stack gas moisture consists of a series of glass impingers connected together in series, preceded by a glass filter holder. The filter holder is housed in a heated sample box, which is controlled from the metering console, and is positioned in-line between the extractive sample probe and the glass impinger train. The box is maintained at a temperature of approximately 250°F to prevent saturation of the filter due to the moisture of the sample gas. During sampling, the process exhaust gas is drawn across the filter, depositing all particulate matter, and proceeds through the impinger train, positioned in an ice bath, where the moisture contained in the process gas is extracted. The first and second impingers in the train are filled with approximately 200 ml of deionized water, while the third impinger remains empty, collecting any remaining uncombined moisture. The fourth and final impinger is filled with silica gel, which desiccates the sample, thereby removing all of the moisture.

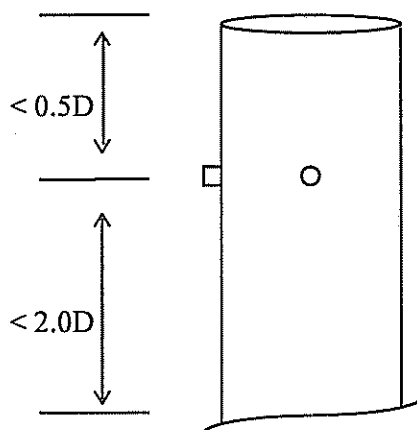
Appendix A

Source Specifications

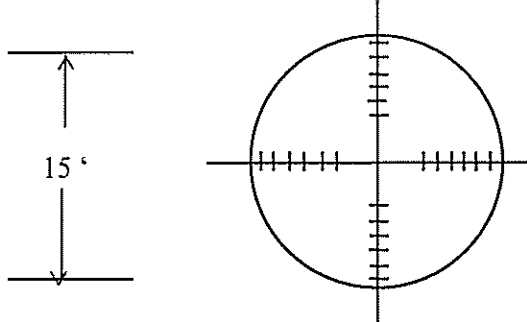
Source Dimensions / Testing Locations
Traverse Point Diagram

**EAF Baghouse # 1
(SN-01)**

SIDE VIEW



TOP VIEW



Point	% Diameter	Distance' in.
1	2.1	3.78
2	6.7	12.06
3	11.8	21.24
4	17.7	31.86
5	25.0	45.0
6	35.6	64.08

* Distance excludes port stand-off

Note: The EAF South Baghouse (# 1) has a round, vertical stack with a 15 ft. diameter. The duct is configured with four accessible ports. Six sampling traverse points were obtained from each port for a total of 24 traverse points as specified.

MacSteel Arkansas
Ft. Smith, AR

Baghouse # 2 (SN-12)
Compartment Size: 28.67' x 19.42'

1	2	3	4	5	6	7
8	9	10	11	12	13	14

The Electric Arc Furnace North Baghouse (# 2) is a positive pressure filter baghouse with 14 compartments with an inside area of 556.77 sq. ft. each. Three EPA Method 5D test runs were conducted consisting of sampling 4 compartments per test run. This strategy therefore included 12 total compartments. Each compartment was sampled for a sixty minute period across 8 traverse points on a 4x2 matrix. Each traverse point was sampled for 7.5 minutes for a total test time of 240 minutes. A minimum of 160 scf were collected per test run.

Appendix B

Field Data Records

Particulate Matter Field Data Records

REFERENCE METHOD 5D

Facility MACSTEEL
 Location _____
 Operator _____
 Date 4-17-07
 Run No. 1
 Sample Box No. NITECH
 Meter Box No. _____
 Meter ΔH _____
 C Factor _____

54-12

Ambient Temp 60
 Barometric Pressure 30.0
 Nozzle Diameter 1.25
 Leak Rate (cfm) 0.1210
 Static Pressure _____
 Filter No. 3268
 Impinger Vol. (initial) 200
 Impinger Vol. (final) 210
 Silica Gel Wt. (initial) 505
 Silica Gel Wt. (final) 540

Inlet SCFM:

Compartment #: 1

Traverse Point No.	Sample Time (min.)	Sample Vacuum (in. Hg)	Stack Temp. (°F)	ΔH in. H ₂ O	Gas Volume (ft ³)	DGM Temp. IN	DGM Temp. OUT	Filter Temp. (°F)	Last Impinger (°F)
1	905	6	134	3.0	704.038	60	59		43
2		7	123	↓		58	58		35
3		8	115			60	58		25
4		9	114			61	58		23
5		9	125			62	58		33
6		9	124			63	59		35
7		9	122			64	60		37
8	1005	9	121		760.9	63	59		38

Compartment #: 2

Traverse Point No.	Sample Time (min.)	Sample Vacuum (in. Hg)	Stack Temp. (°F)	ΔH in. H ₂ O	Gas Volume (ft ³)	DGM Temp. IN	DGM Temp. OUT	Filter Temp. (°F)	Last Impinger (°F)
1	1010	9	123	3.0	760.9	60	59		39
2		9	125	↓		61	58		33
3		9	123			62	57		30
4		10	122			63	57		27
5		10	115			62	55		27
6		10	114			61	53		25
7		10	119			62	55		34
8	1110	10	118		819.4	63	55		34

Compartment #: 3

Traverse Point No.	Sample Time (min.)	Sample Vacuum (in. Hg)	Stack Temp. (°F)	ΔH in. H ₂ O	Gas Volume (ft ³)	DGM Temp. IN	DGM Temp. OUT	Filter Temp. (°F)	Last Impinger (°F)
1	1015	10	111	3.0	819.4	61	57		38
2		10	115	↓		63	57		34
3		10	119			62	55		34
4		10	124			63	56		35
5		10	125			63	56		36
6		10	123			64	57		38
7		10	122			65	57		39
8	1215	10	121		878.5	65	57		39

SN-12

Inlet SCFM:

Facility MASTEEL
Location _____
Operator _____
Date 4-17-07
Run No. 1 cont.
Sample Box No. _____
Meter Box No. _____
Meter Δ H. _____
C Factor _____

Ambient Temp _____
 Barometric Pressure _____
 Nozzle Diameter _____
 Leak Rate (cfm) _____
 Static Pressure _____
 Filter No. _____
 Impinger Vol. (initial) _____
 Impinger Vol. (final) _____
 Silica Gel Wt. (initial) _____
 Silica Gel Wt. (final) _____

Inlet SCFM:

Traverse Point No.	Sample Time (min.)	Sample Vacuum (in. Hg)	Stack Temp. (°F)	ΔH in. H ₂ O	Gas Volume (ft ³)	DGM Temp. IN	DGM Temp. OUT	Filter Temp. (°F)	Last Impinger (°F)
1	1220	10	122	3.0	878.5	62	59		44
2		10	124	6		64	60		39
3		10	124			64	59		42
4		10	120			64	59		44
5		10	121			64	58		45
6		10	119			64	58		46
7		10	120			64	58		47
8	1320	10	122		937.574	64	58		47

[illegible][illegible]

REFERENCE METHOD 5D

Facility Massey
 Location St. Smith, AR
 Operator JS
 Date 4-17-67
 Run No. 2
 Sample Box No. _____
 Meter Box No. _____
 Meter ΔH _____
 C Factor _____

Inlet SCFM:

Ambient Temp 65
 Barometric Pressure 30.0
 Nozzle Diameter _____
 Leak Rate (cfm) 0.01 @ 15"
 Static Pressure _____
 Filter No. R-3363
 Impinger Vol. (initial) 200
 Impinger Vol. (final) 204
 Silica Gel Wt. (initial) 520
 Silica Gel Wt. (final) 555

Compartment #: 6

Traverse Point No.	Sample Time (min.)	Sample Vacuum (in. Hg)	Stack Temp. (°F)	ΔH in. H ₂ O	Gas Volume (ft ³)	DGM Temp. IN	DGM Temp. OUT	Filter Temp. (°F)	Last Impinger (°F)
1	1420	8	114	2.6	937.715	54	53		56
2		8	116	↓		57	55		56
3		8	120			59	55		55
4		8	116			59	54		52
5		9	115			60	56		52
6		9				62			53
7		9				63			53
8	1520	9			992.8	64	57		54

Compartment #: 5

Traverse Point No.	Sample Time (min.)	Sample Vacuum (in. Hg)	Stack Temp. (°F)	ΔH in. H ₂ O	Gas Volume (ft ³)	DGM Temp. IN	DGM Temp. OUT	Filter Temp. (°F)	Last Impinger (°F)
1	1525	9	123	2.6	992.8	60	57		56
2		9	122	↓		63	60		54
3		9	127			63	58		54
4		9	127			64	61		54
5		9	125			64	60		54
6		9	124			65	60		54
7		9	122			65	60		54
8	1625	9	121		1047.9	65	60		54

Compartment #: 13

Traverse Point No.	Sample Time (min.)	Sample Vacuum (in. Hg)	Stack Temp. (°F)	ΔH in. H ₂ O	Gas Volume (ft ³)	DGM Temp. IN	DGM Temp. OUT	Filter Temp. (°F)	Last Impinger (°F)
1	1630	9	120	2.6	1047.9	63	58		55
2	↓	9	121	↓		64	58		46
3		9	121			65	58		43
4		9	120			65	58		43
5		9	119			65	58		42
6		9	119			65	58		42
7		9	114			65	58		41
8	1730	9	113		1042.8	65	58		40

Facility MACASTEEL
Location _____
Operator _____
Date 4-17-07
Run No. 2 CONT
Sample Box No. _____
Meter Box No. _____
Meter ΔH_n _____
C Factor _____

Inlet SCFM:

Ambient Temp _____
Barometric Pressure _____
Nozzle Diameter _____
Leak Rate (cfm) _____
Static Pressure _____
Filter No. _____
Impinger Vol. (initial) _____
Impinger Vol. (final) _____
Silica Gel Wt. (initial) _____
Silica Gel Wt. (final) _____

Traverse Point No.	Sample Time (min.)	Sample Vacuum (in. Hg)	Stack Temp. (°F)	ΔH in. H ₂ O	Gas Volume (ft ³)	DGM Temp. IN	DGM Temp. OUT	Filter Temp. (°F)	Last Inupinger (°F)
1	1735	9	106	2.6	1102.8	63	66		46
2		9	113	↓		65	58		41
3		9	114			65	58		40
4		9	114			65	58		42
5		9	110			65	58		44
6		9	112			65	58		46
7		9				65	58		47
8	1835	7			1157.741	65	58		49

[illegible][illegible]

REFERENCE METHOD 5D

Facility MARSHALL
 Location East Smith, AR
 Operator 15
 Date 4-18-07
 Run No. 3
 Sample Box No. _____
 Meter Box No. _____
 Meter Δ H₂ _____
 C Factor _____

SN-12

Inlet SCFM:

Ambient Temp 60
 Barometric Pressure 29.8
 Nozzle Diameter 1.25
 Leak Rate (cfm) 0.01 @ 10'
 Static Pressure _____
 Filter No. R-3364
 Impinger Vol. (initial) 200
 Impinger Vol. (final) 216
 Silica Gel Wt. (initial) 465
 Silica Gel Wt. (final) 505

Compartment #: 811

Traverse Point No.	Sample Time (min.)	Sample Vacuum (in. Hg)	Stack Temp. (°F)	ΔH in. H ₂ O	Gas Volume (ft ³)	DGM Temp. IN	DGM Temp. OUT	Filter Temp. (°F)	Last Impinger (°F)
1	930	6	102	2.6	158.040	57	58		47
2		6	119	↓		61	63		44
3		6	118	↓		62	63		45
4		7	124	↓		64	64		48
5		6	123			63	63		50
6		6	124			64	62		52
7		6	131			64	61		53
8	1030	6	134		211.5	64	61		52

Compartment #: 10

Traverse Point No.	Sample Time (min.)	Sample Vacuum (in. Hg)	Stack Temp. (°F)	ΔH in. H ₂ O	Gas Volume (ft ³)	DGM Temp. IN	DGM Temp. OUT	Filter Temp. (°F)	Last Impinger (°F)
1	1035	6	130	2.6	211.5	65	61		50
2		6	135	↓		64	59		51
3		6	133	↓		62	59		52
4		6	132			63	58		53
5		6	130			63	58		54
6		6	128			63	58		47
7		6	126			63	58		46
8	1135	6	125		264.7	63	58		48

Compartment #: 9

Traverse Point No.	Sample Time (min.)	Sample Vacuum (in. Hg)	Stack Temp. (°F)	ΔH in. H ₂ O	Gas Volume (ft ³)	DGM Temp. IN	DGM Temp. OUT	Filter Temp. (°F)	Last Impinger (°F)
1	1140	6	123	2.6	264.7	65	60		52
2		7	126	↓		64	58		48
3		7	129	↓		63	56		45
4		7	128	↓		62	55		45
5		7	127			63	54		41
6		7	123			63	54		42
7		7	114			63	55		41
8	1240	7	119		318.5	63	66		43

Inlet SCFM:

Facility MACSTEEL
Location _____
Operator JS
Date 4-19-07
Run No. 3 cont
Sample Box No. _____
Meter Box No. _____
Meter ΔH_a _____
C Factor _____

Ambient Temp _____
Barometric Pressure _____
Nozzle Diameter _____
Leak Rate (cfm) _____
Static Pressure _____
Filter No. _____
Impinger Vol. (initial) _____
Impinger Vol. (final) _____
Silica Gel Wt. (initial) _____
Silica Gel Wt. (final) _____

Compartment #: 4

Traverse Point No.	Sample Time (min.)	Sample Vacuum (in. Hg)	Stack Temp. (°F)	ΔH in. H ₂ O	Gas Volume (ft ³)	DGM Temp. IN	DGM Temp. OUT	Filter Temp. (°F)	Last Impinger (°F)
1	1245	7	116	26	313.5	65	60		47
2		7	120	↓		65	56		42
3		7	118	↓		63	58		42
4		7	121			63	58		43
5		7	118			64	58		45
6		7	118			63	57		45
7		7	119			63	57		46
8	1345	7	119		372.971	63	57		46

Compartment #:

[illegible]

Compartment #:

[illegible]

Current Time : 13:33

Daily Parameter Report - Minute Averages with Flags
MacSteel

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Logger Name : MACSTEEL
Logger Id   : 01
Parameter   : 2FLOWRAT
Units       : SCFM

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Stack      :
Boiler/Unit :
Interval   : 001M
```

Date	Time	Average	Data Flags <PDTFBCMOUA+-RHLhlJjVWXYZf	Status Flags I?*>=m^vEd9za Q
04/17/07	08:00	798149		
04/17/07	08:01	797575		
04/17/07	08:02	803954		
04/17/07	08:03	817457		
04/17/07	08:04	830821		
04/17/07	08:05	819022		
04/17/07	08:06	806203		
04/17/07	08:07	793279		
04/17/07	08:08	795963		
04/17/07	08:09	800046		
04/17/07	08:10	787990		
04/17/07	08:11	789322		
04/17/07	08:12	797381		
04/17/07	08:13	791684		
04/17/07	08:14	783649		
04/17/07	08:15	779451		
04/17/07	08:16	782628		
04/17/07	08:17	783111		
04/17/07	08:18	780277		
04/17/07	08:19	779654		
04/17/07	08:20	784055		
04/17/07	08:21	779923		
04/17/07	08:22	778257		
04/17/07	08:23	772088		
04/17/07	08:24	776477		
04/17/07	08:25	771604		
04/17/07	08:26	769072		
04/17/07	08:27	782628		
04/17/07	08:28	781301		
04/17/07	08:29	773053		
04/17/07	08:30	774087		
	Max	830821		
	Min	769072		
	Mean	789044		
	Records	31		

[illegible]

Current Date : 04/17/07
Current Time : 13:34

Daily Parameter Report - Minute Averages with Flags
MacSteel

Logger Name : MACSTEEL
Logger Id : 01
Parameter : 2FLOWRAT
Units : SCFM

Stack :
Boiler/Unit :
Interval : 001M

Date	Time	Average	Data Flags <PDTFBCMOUA+-RHLhlJjVWXYZf	Status Flags I?*>=m^vEd9za Q
04/17/07	13:00	781455		
04/17/07	13:01	786730		
04/17/07	13:02	785308		
04/17/07	13:03	782999		
04/17/07	13:04	781851		
04/17/07	13:05	774177		
04/17/07	13:06	772893		
04/17/07	13:07	770444		
04/17/07	13:08	772938		
04/17/07	13:09	761980		
04/17/07	13:10	767120		
04/17/07	13:11	771487		
04/17/07	13:12	756967		
04/17/07	13:13	763296		
04/17/07	13:14	760308		
04/17/07	13:15	756567		
04/17/07	13:16	757692		
04/17/07	13:17	757225		
04/17/07	13:18	758993		
04/17/07	13:19	754593		
04/17/07	13:20	752144		
04/17/07	13:21	750787		
04/17/07	13:22	747690		
04/17/07	13:23	744898		
04/17/07	13:24	753279		
04/17/07	13:25	747438		
04/17/07	13:26	744022		
04/17/07	13:27	744045		
04/17/07	13:28	743374		
04/17/07	13:29	745719		
04/17/07	13:30	754450		
	Max	786730		
	Min	743374		
	Mean	761383		
	Records	31		

status : '<' - Less than ##- Data, 'P' - Power Fail, 'D' - Disabled, 'T' - Out-
-Control, 'F' - Boiler Off-Line,
Flags : 'B' - Bad Status, 'C' - Calibration, 'M' - Maintenance, 'O' -
Analog Overrange, 'U' - Analog Underrange,
'A' - Arithmetic Error, '+' - Maximum, '-' - Minimum, 'R' - Rate
Change, 'H' - High-High Alarm,
'L' - Low-Low Alarm, 'h' - High Alarm, 'l' - Low Alarm, 'J' - High
Rate of Change, 'j' - Low Rate of Change,
'V' - DIS #1 Obs, 'W' - DIS #2 Obs, 'X' - DIS #3 Obs, 'Y' - DIS
Obs, 'Z' - DIS #5 Obs.

MD401
Revised 11-15-04
By WET

Current Date : 04/18/07
Current Time : 11:09

Daily Parameter Report - Minute Averages with Flags
MacSteel

Logger Name : MACSTEEL
Logger Id : 01
Parameter : 2FLOWRAT
Units : SCFM

Stack :
Boiler/Unit :
Interval : 001M

Date	Time	Average	Data Flags <PDTFBCMOUA+-RHLhIJjVWXYZf	Status Flags I?*>=m^vEd9za Q
04/18/07	08:30	759502		
04/18/07	08:31	757816		
04/18/07	08:32	758394		
04/18/07	08:33	758927		
04/18/07	08:34	757723		
04/18/07	08:35	769570		
04/18/07	08:36	750758		
04/18/07	08:37	751183		
04/18/07	08:38	768534		
04/18/07	08:39	770208		
04/18/07	08:40	766938		
04/18/07	08:41	766182		
04/18/07	08:42	768878		
04/18/07	08:43	767441		
04/18/07	08:44	768074		
04/18/07	08:45	764982		
04/18/07	08:46	773198		
04/18/07	08:47	765632		
04/18/07	08:48	766982		
04/18/07	08:49	774313		
04/18/07	08:50	768537		
04/18/07	08:51	768294		
04/18/07	08:52	768691		
04/18/07	08:53	770379		
04/18/07	08:54	777162		
04/18/07	08:55	770338		
04/18/07	08:56	764757		
04/18/07	08:57	748853		
04/18/07	08:58	738642		
04/18/07	08:59	748269		
04/18/07	09:00	752309		
	Max	777162		
	Min	738642		
	Mean	763273		
	Records	31		

Status : '<' - Less than ##* Data, 'P' - Power Fail, 'D' - Disabled, 'T' - Out-of-Control, 'F' - Boiler Off-Line,
Flags : 'B' - Bad Status, 'C' - Calibration, 'M' - Maintenance, 'O' - Analog Overrange, 'U' - Analog Underrange,
'A' - Arithmetic Error, '+' - Maximum, '-' - Minimum, 'R' - Rate of Change, 'H' - High-High Alarm,
'L' - Low-Low Alarm, 'h' - High Alarm, 'l' - Low Alarm, 'J' - High Rate of Change, 'j' - Low Rate of Change,
'V' - DIS #1 Obs, 'W' - DIS #2 Obs, 'X' - DIS #3 Obs, 'Y' - DIS #4 Obs, 'Z' - DIS #5 Obs.

Facility Max Steel
 Location At. Smith AR
 Operator JS
 Date 4-19-07
 Run No. 1
 Sample Box No. _____
 Meter Box No. _____
 Meter ΔH _____
 C Factor _____
 Pitot Coeff (C_p) _____

SN-01

Diameter (in.) _____
 Downstream (in.) _____
 Upstream (in.) _____

Ambient Temp 55
 Barometric Pressure 30.0
 Nozzle Diameter 0.24
 Leak Rate (cfm) 0.01 @ 10"
 Static Pressure 0.3
 Filter No. R-3365
 Impinger Vol. (initial) 200
 Impinger Vol. (final) 205
 Silica Gel Wt. (initial) 490
 Silica Gel Wt. (final) 520

Initial Meter Reading: 373.190

Traverse Point No.	Sample Time (min.)	Sample Vacuum (in. Hg)	Stack Temp. (°F)	ΔP in. H ₂ O	ΔH in. H ₂ O	Gas Volume (ft ³)	DGM Temp. IN	DGM Temp. OUT	Filter Temp. (°F)	Last Impinger (°F)
1	850 850	2	110	.30	1.0	378.6	58	56		57
2	900	2	105	.55	1.9	386.1	60	55		56
3	916	4	103	.80	2.7	394.8	63	53		45
4	920	3	99	.40	1.4	401.3	64	52		43
5	930	3	102	.35	1.2	407.5	63	52		41
6	940	3	99	.35	1.2	413.6	63	53		41
7	950 950	2	102	.25	0.9	418.9	57	53		47
8	1010	2	101	.25	0.9	424.3	61	54		40
9	1020	3	101	.35	1.2	430.5	61	54		41
10	1030	3	98	.45	1.5	437.3	62	55		40
11	1040	3	103	.55	1.9	445.0	62	53		37
12	1050	4	98	.60	2.0	452.8	63	54		37
13	1060 1060	2	99	.25	0.9	458.2	58	53		42
14	1120	3	98	.35	1.2	464.3	59	54		35
15	1130	3	99	.45	1.5	471.0	59	53		34
16	1140	3	101	.45	1.5	478.4	60	54		33
17	1150	3	101	.60	2.0	486.3	60	55		32
18	1200	3	99	.40	1.4	493.0	62	56		32
19	1205 1205	3	101	.45	1.5	499.8	58	55		35
20	1225	3	104	.55	1.9	507.5	59	55		32
21	1235	3	106	.50	1.7	515.0	60	55		31
22	1245	3	98	.55	1.9	522.6	60	54		33
23	1255	3	97	.60	2.0	530.7	60	55		33
24	1305	3	100	.65	2.2		61	55		35

Final Meter Reading: 539.115

Facility Macsteel
 Location Fort Smith
 Operator JS
 Date 4-19-07
 Run No. 2
 Sample Box No. _____
 Meter Box No. _____
 Meter ΔH_u _____
 C Factor _____
 Pitot Coeff (C_p) _____

5N-01

Diameter (in.) _____
 Downstream (in.) _____
 Upstream (in.) _____

Ambient Temp 65
 Barometric Pressure 30.0
 Nozzle Diameter 0.24
 Leak Rate (cfm) 0.0010
 Static Pressure 0.4
 Filter No. R-
 Impinger Vol. (initial) 200
 Impinger Vol. (final) 205
 Silica Gel Wt. (initial) 505
 Silica Gel Wt. (final) 540

Initial Meter Reading: 540.029

Traverse Point No.	Sample Time (min.)	Sample Vacuum (in. Hg)	Stack Temp. (°F)	ΔP in. H ₂ O	ΔH in. H ₂ O	Gas Volume (ft ³)	DGM Temp. IN	DGM Temp. OUT	Filter Temp. (°F)	Last Impinger (°F)
1	1350 1400	2	102	.30	1.0	545.7	56	54		47
2	1410	2	100	.40	1.4	552.3	56	54		53
3	1420	3	103	.55	1.9	560.1	60	53		49
4	1430	3	96	.65	2.2	569.0	60	52		45
5	1440	3	95	.65	2.2	577.0	61	52		42
6	1450	3	94	.65	2.2	585.4	61	52		41
7	1455 1505	2	93	.35	1.2	591.5	58	53		40
8	1515	3	101	.45	1.5	598.6	58	53		43
9	1525	3	93	.55	1.9	606.4	59	53		44
10	1535	4	95	.65	2.2	614.9	59	53		45
11	1545	3	94	.60	2.0	622.8	59	53		46
12	1555	3	97	.60	2.0	630.7	59	53		46
13	1600 1615	3	96	.35	1.2	637.1	58	53		47
14	1620	3	95	.55	1.9	645.3	58	53		46
15	1630	3	95	.55	1.9	653.0	59	52		46
16	1640	3	94	.55	1.9	660.3	60	52		46
17	1650	3	96	.45	1.5	667.5	60	52		47
18	1700	3	94	.45	1.5	674.6	59	53		46
19	1707 1715	3	98	.35	1.2	680.8	58	53		43
20	1725	3	101	.55	1.9	688.6	59	54		45
21	1735	3	101	.60	2.0	696.5	60	54		46
22	1745	3	100	.65	2.2	704.9	60	54		47
23	1755	3	99	.60	2.0	713.0	60	54		49
24	1805	3	98	.60	2.0		61	54		50

Final Meter Reading: 720.861

Facility MACSteel
 Location FA Smith
 Operator JS
 Date 4-20-07
 Run No. 3
 Sample Box No. _____
 Meter Box No. _____
 Meter ΔH _____
 C Factor _____
 Pitot Coeff (C_p) _____

SN-01

Diameter (in.) _____
 Downstream (in.) _____
 Upstream (in.) _____

Ambient Temp 55
 Barometric Pressure 30.0
 Nozzle Diameter 0.24
 Leak Rate (cfm) _____
 Static Pressure 0.3
 Filter No. _____
 Impinger Vol. (initial) 200
 Impinger Vol. (final) 205
 Silica Gel Wt. (initial) 905
 Silica Gel Wt. (final) 525

Initial Meter Reading: 721.029

Traverse Point No.	Sample Time (min.)	Sample Vacuum (in. Hg)	Stack Temp. (°F)	ΔP in. H ₂ O	ΔH in. H ₂ O	Gas Volume (ft ³)	DGM Temp. IN	DGM Temp. OUT	Filter Temp. (°F)	Last Impinger (°F)
1	825 845	2	115	.30	1.0	726.8	59	57		57
2	845	2	112	.40	1.4	733.6	59	56		56
3	855	3	109	.60	2.0	740.8	62	57		54
4	905	3	109	.65	2.2	749.0	63	55		55
5	915	3	110	.65	2.2	752.1	64	55		54
6	925	3	106	.65	2.2	765.0	64	55		53
7	930 940	3	105	.35	1.2	770.5	63	54		53
8	950	3	104	.40	1.4	777.6	63	54		54
9	1000	3	105	.50	1.7	784.7	61	54		54
10	1010	3	102	.60	2.0	792.8	62	54		53
11	1020	3	99	.65	2.2	801.0	62	54		53
12	1030	3	98	.65	2.2	809.2	62	53		51
13	1033 1045	3	98	.30	1.0	815.9	59	53		48
14	1055	3	99	.45	1.5	822.0	59	52		45
15	1105	3	99	.45	1.5	828.8	59	52		41
16	1115	3	101	.50	1.7	836.2	59	53		40
17	1125	3	102	.60	2.0	843.6	59	53		40
18	1135	3	104	.60	2.0	851.9	60	54		42
19	1140 1150	2	99	.30	1.0	857.8	57	53		43
20	1200	3	100	.45	1.5	864.6	57	53		44
21	1210	3	102	.55	1.9	872.4	58	53		45
22	1220	3	99	.55	1.9	880.3	58	53		46
23	1230	3	99	.60	2.0	888.3	58	53		47
24	1240	3	98	.60	2.0		58	53		47

Final Meter Reading: 896.116

Appendix C

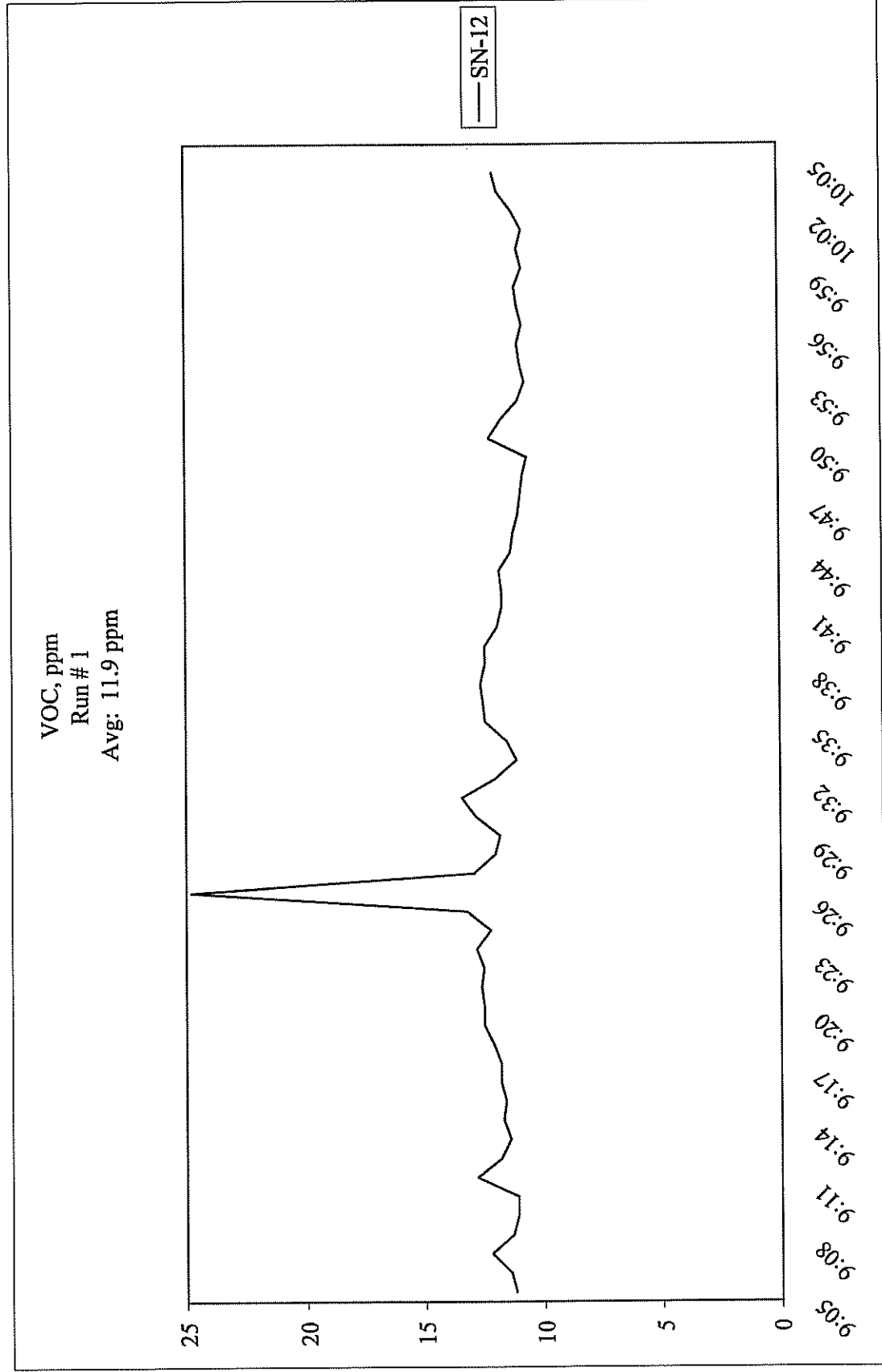
Analysis Data

Volatile Organic Compound Results
Particulate Matter Gravimetric Analysis

MacSteel
Ft. Smith, AR

EAF Exhaust
(SN-12)

April 17, 2007

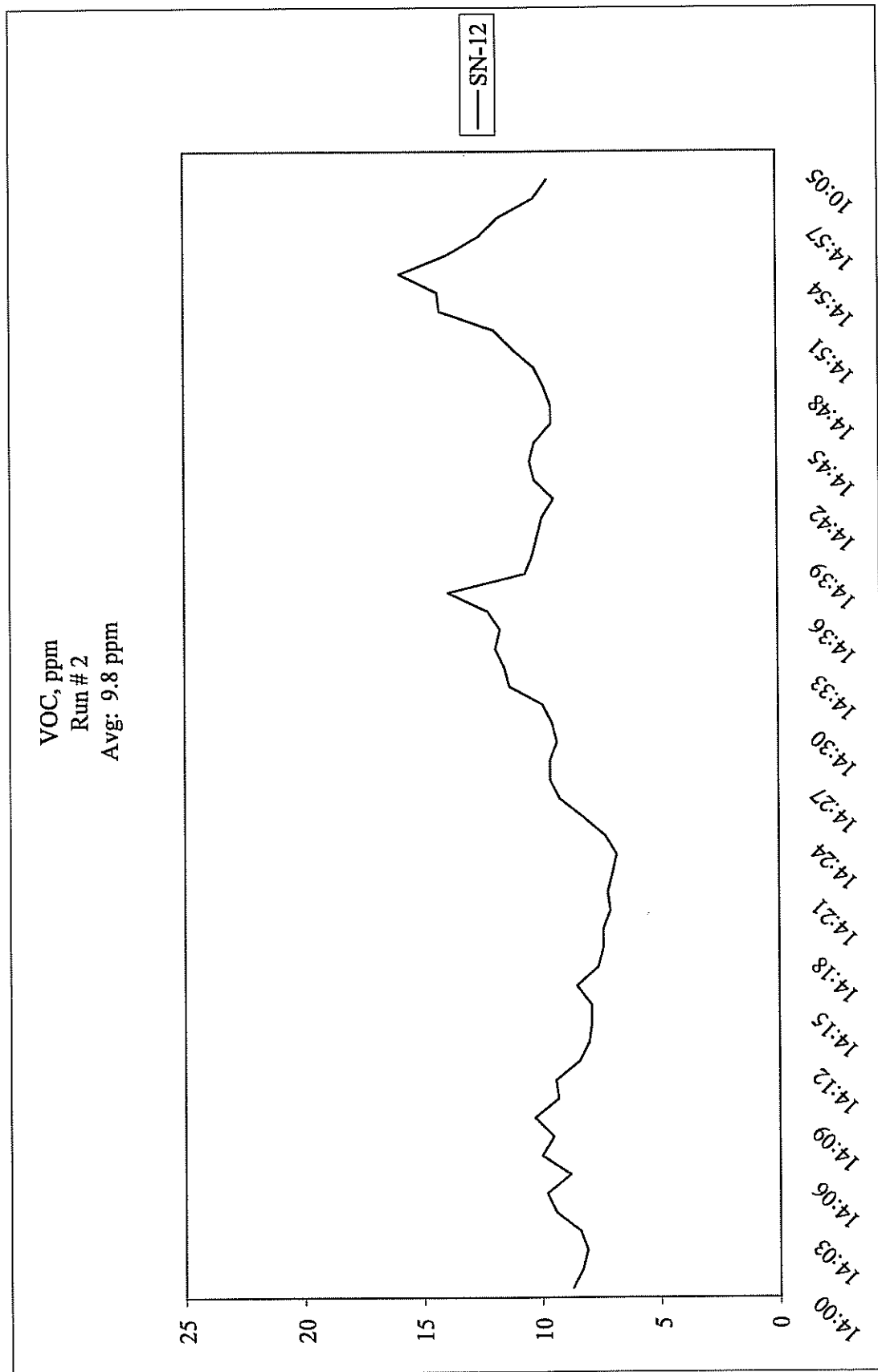


White Star Environmental

MacSteel
Ft. Smith, AR

EAF Exhaust
(SN-12)

April 17, 2007

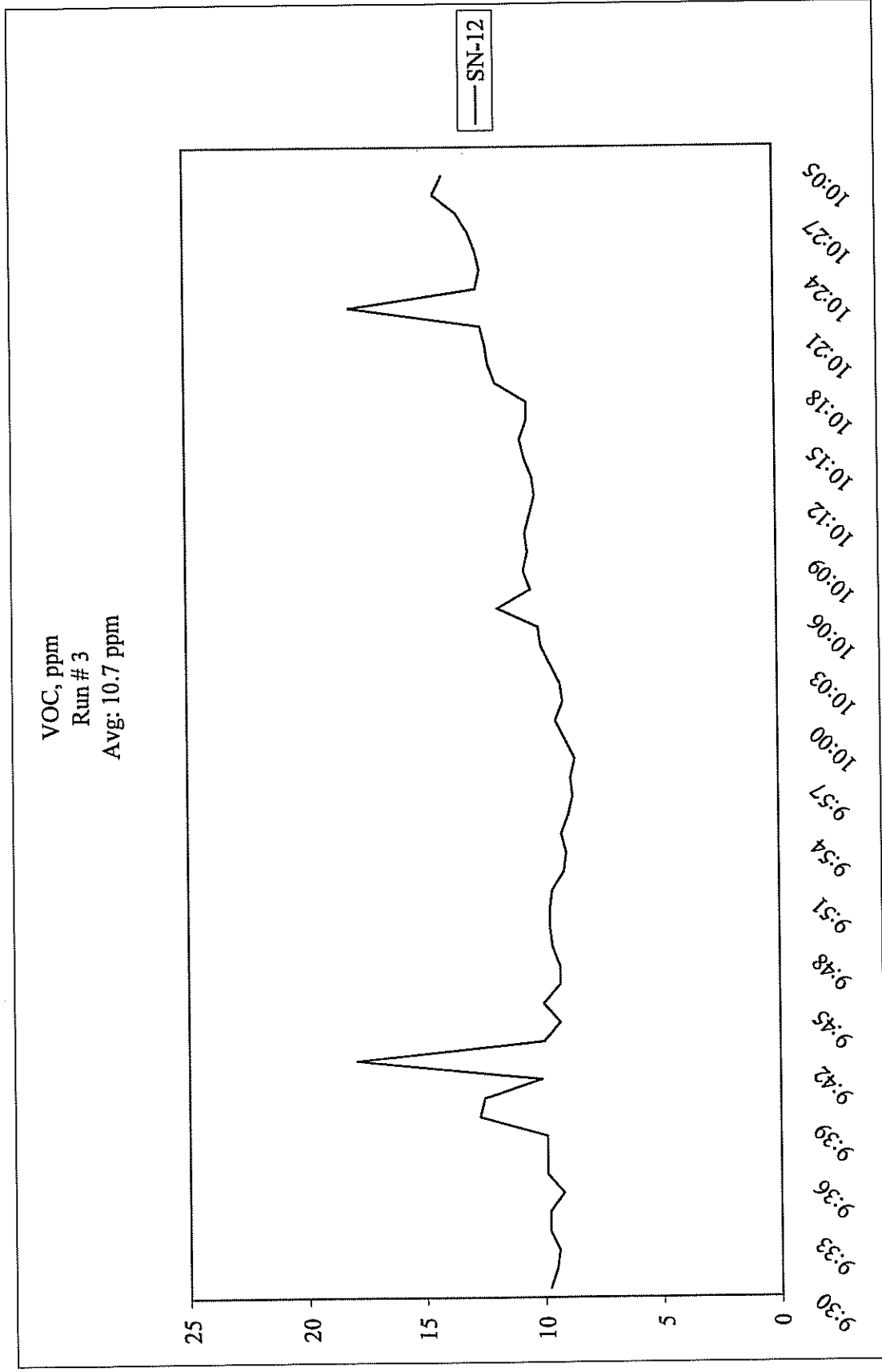


White Star Environmental

MacSteel
Ft. Smith, AR

EAF Exhaust
(SN-12)

April 17, 2007

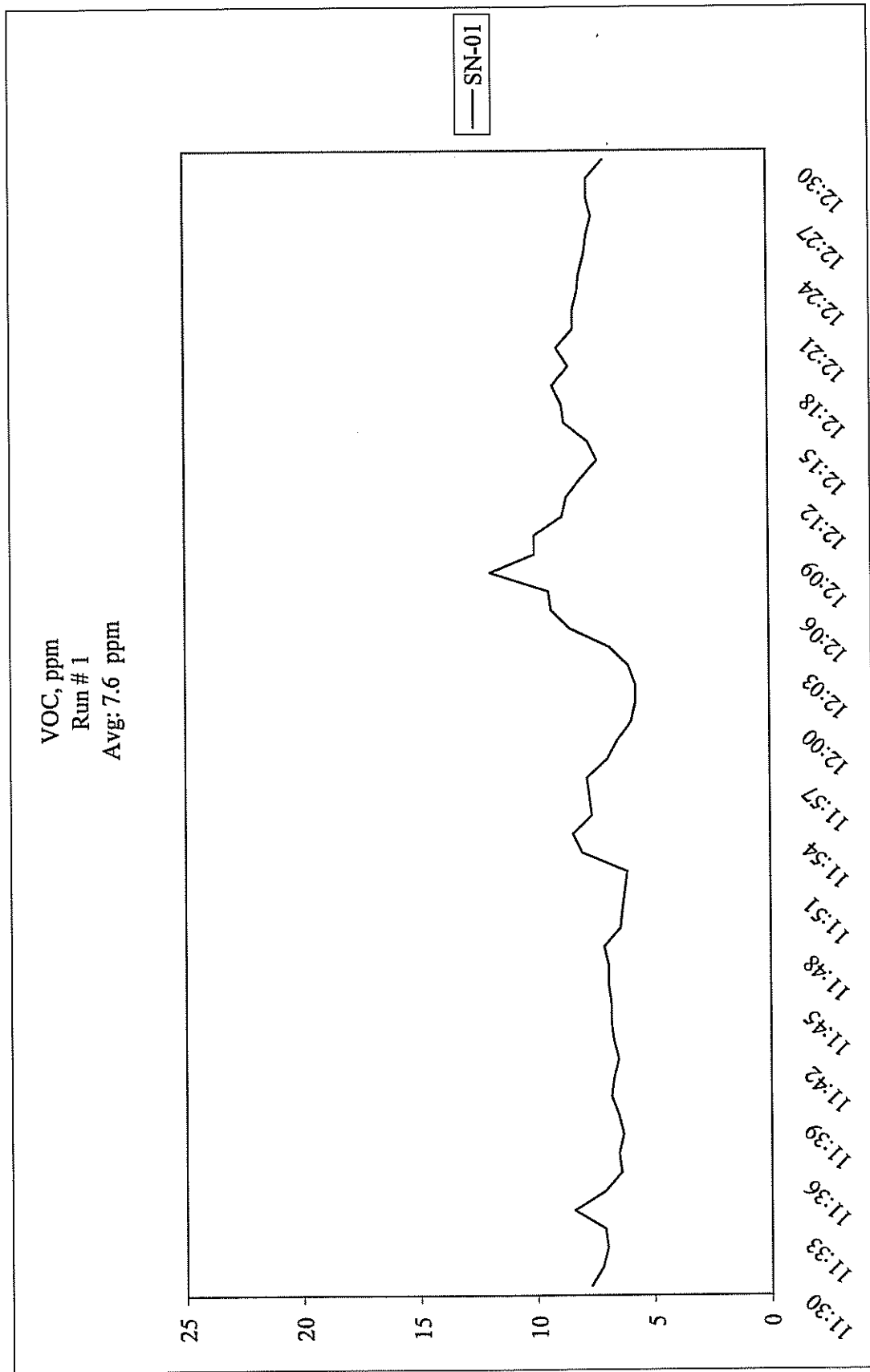


White Star Environmental

MacSteel
Ft. Smith, AR

EAF Exhaust
(SN-01)

April 19, 2007

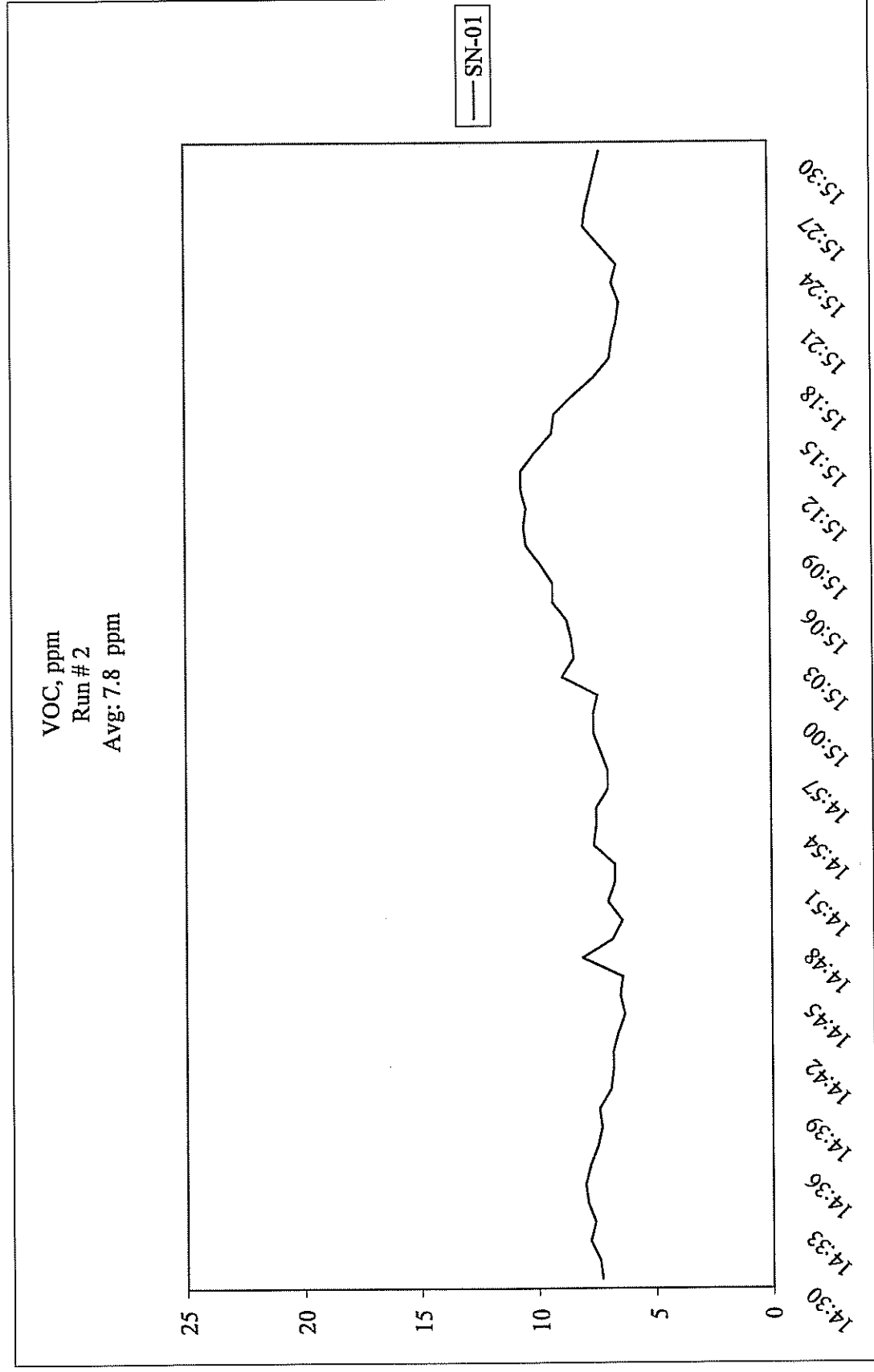


White Star Environmental

MacSteel
Ft. Smith, AR

EAF Exhaust
(SN-01)

April 19, 2007

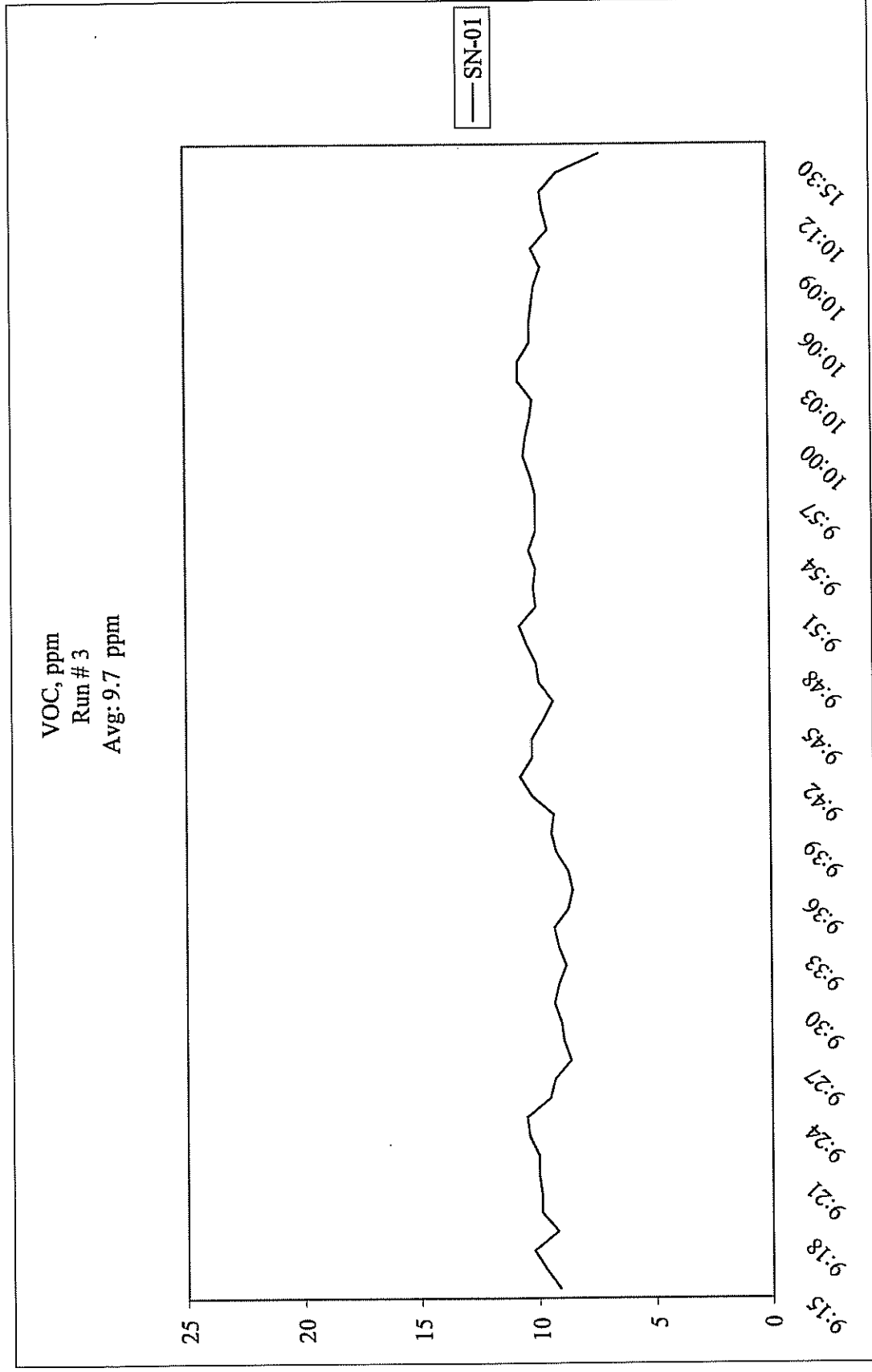


White Star Environmental

MacSteel
Ft. Smith, AR

EAFF Exhaust
(SN-01)

April 20, 2007



White Star Environmental

Gravimetric Analysis Report

MacSteel Corp.
EAF #1 (SN-01)

Acetone Blank Sample			
Volume, ml	100	Date/Time	
1st weight	54.7969	4/29; 10:00	
2nd weight	54.797	4/30; 16:00	
Average	54.79695		
Tare Wt.	54.7964		
Blank Wt.	0.0005		
Filter Samples			
Item	Run 1	Run 2	Run 3
Filter No.	R-3365	R-3366	R-3367
1st weight	0.3753	0.3772	0.3809
2nd weight	0.3752	0.3772	0.381
Average	0.37525	0.3772	0.38095
Tare Wt.	0.3723	0.3746	0.3781
Wt. of PM	0.00295	0.0026	0.00285
Acetone Wash Samples			
Item	Run 1	Run 2	Run 3
Volume, ml	120	140	110
1st weight	54.5092	54.391	55.0758
2nd weight	54.509	54.3912	55.0758
Average	54.5091	54.3911	55.0758
Tare Wt.	54.5061	54.3892	55.0735
Blank Wt.	0.0007	0.0008	0.0006
Wt. of PM	0.0023	0.0011	0.0017
Particulate Matter, mg			
Filter Wt.	2.9	2.6	2.9
Acetone Wt.	2.3	1.1	1.7
Total Wt.	5.3	3.7	4.5

Analyst: wjs

Hygrometer: 32 %

White Star Environmental

Gravimetric Analysis Report

MacSteel Corp.
EAF #2 (SN-12)

Acetone Blank Sample			
Volume, ml	100	Date/Time	
1st weight	54.7969	4/29; 10:00	
2nd weight	54.797	4/30; 16:00	
Average	54.79695		
Tare Wt.	54.7964		
Blank Wt.	0.0005		
Filter Samples			
Item	Run 1	Run 2	Run 3
Filter No.	3268	R-3363	R-3364
1st weight	0.2588	0.3778	0.3817
2nd weight	0.259	0.3777	0.3815
Average	0.2589	0.37775	0.3816
Tare Wt.	0.2569	0.3732	0.3794
Wt. of PM	0.002	0.00455	0.0022
Acetone Wash Samples			
Item	Run 1	Run 2	Run 3
Volume, ml	85	90	90
1st weight	54.9158	55.3936	54.4369
2nd weight	54.9158	55.3934	54.437
Average	54.9158	55.3935	54.4370
Tare Wt.	54.9131	55.3903	54.4349
Blank Wt.	0.0005	0.0005	0.0005
Wt. of PM	0.0022	0.0027	0.0016
Particulate Matter, mg			
Filter Wt.	2.0	4.6	2.2
Acetone Wt.	2.2	2.7	1.6
Total Wt.	4.2	7.3	3.8

Analyst: wjs

Hygrometer: 32 %

White Star Environmental

Appendix D

Calibration

Calibration Standard Cert. of Analysis
Instrument Calibration Records
Isokinetic Equipment Calibration

Certificate of Analysis

EPA Protocol

Performed according to EPA-600/R-97/121, Procedure G1

Notice: This Cylinder is not to be used when pressure is under 150 psig.

Manufactured and certified at:

Linde Gas LLC
Maumee Specialty Gas Plant
6421 Monclova Road
MAUMEE OH 43537
419-893-7226

Produced for customer:

LINDE MEMPHIS INTERBRANCH
3390 WINBROOK
MEMPHIS TN 38116
USA
901-396-7020

Material:	5982		Blend Tolerance:	5 % Relative
EPA CH ₄ /N ₂ 0.5 - 130 ppm		A31	Blend Type:	EPA Protocol
Production #:	100111715		Cyl. Pressure:	2000 psig
Lot #:	02499A6070SG		Balance Gas:	Nitrogen
Cylinder #:	CC13630		CGA:	350
Expiration Date:	1/12/2009		Analytical Accuracy:	1.00 % Relative
Shelf Life:	36 months		Confidence:	95 %

CAS #	Certified Component	Requested Concentration	Concentration and Uncertainty	Date of Certification
74-82-8	Methane	85	86.2 +/- 0.9 ppm	01/12/2006
7727-37-9	Nitrogen		Balance	01/12/2006

CAS #	Reference Standard	Cylinder/Standard #	Concentration	Expire Date
74-82-8	Methane	CC24916 , GMIS	50.23 ppm	07/14/2007
74-82-8	Methane	CC7340 , GMIS	101.4 ppm	06/22/2006

Instrument	Serial #	Analytical Principle	Calibration Date
Horiba FIA-510	56847471	Flame Ionization	01/10/2006

All analyses are performed under controlled environmental conditions. This product is manufactured using equipment which has been calibrated with NIST traceable, or equivalent, standards, weights, or equipment.

Analytical report approved by Roy Yoder

Roy Yoder

Analysis Certificate

Certificate of Analysis

EPA Protocol

Performed according to EPA-600/R-97/121, Procedure G1

Notice: This Cylinder is not to be used when pressure is under 150 psig.

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MAUMEE OH 43537
419-893-7226

Produced for customer:

LINDE MEMPHIS INTERBRANCH
3390 WINBROOK
MEMPHIS TN 38116
USA
901-396-7020

Material:	5982		Blend Tolerance:	5 % Relative
EPA CH ₄ /N ₂ 0.5 - 130 ppm		A31	Blend Type:	EPA Protocol
Production #:	100111715		Cyl. Pressure:	2000 psig
Lot #:	02499A6070SG		Balance Gas:	Nitrogen
Cylinder #:	CC13630		CGA:	350
Expiration Date:	1/12/2009		Analytical Accuracy:	1.00 % Relative
Shelf Life:	36 months		Confidence:	95 %

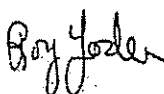
CAS #	Certified Component	Requested Concentration	Concentration and Uncertainty	Date of Certification
74-82-8	Methane	50	50.1 +/- 0.5 ppm	01/12/2006
7727-37-9	Nitrogen		Balance	01/12/2006

CAS #	Reference Standard	Cylinder/Standard #	Concentration	Expire Date
74-82-8	Methane	CC24916 , GMIS	50.23 ppm	07/14/2007
74-82-8	Methane	CC7340 , GMIS	101.4 ppm	06/22/2006

Instrument	Serial #	Analytical Principle	Calibration Date
Horiba FIA-510	56847471	Flame Ionization	01/10/2006

All analyses are performed under controlled environmental conditions. This product is manufactured using equipment which has been calibrated with NIST traceable, or equivalent, standards, weights, or equipment.

Analytical report approved by Roy Yoder



Certificate of Analysis

EPA Protocol

Performed according to EPA-600/R-97/121, Procedure G1

Notice: This Cylinder is not to be used when pressure is under 150 psig.

Manufactured and certified at:

Linde Gas LLC
Maumee Specialty Gas Plant
6421 Monclova Road
MAUMEE OH 43537
419-893-7226

Produced for customer:

LINDE MEMPHIS INTERBRANCH
3390 WINBROOK
MEMPHIS TN 38116
USA
901-396-7020

Material:	5982		Blend Tolerance:	5 % Relative
EPA CH4/N2 0.5 - 130 ppm		A31	Blend Type:	EPA Protocol
Production #:	100111716		Cyl. Pressure:	2000 psig
Lot #:	02499A6070SE		Balance Gas:	Nitrogen
Cylinder #:	CC185422		CGA:	350
Expiration Date:	1/12/2009		Analytical Accuracy:	1.00 % Relative
Shelf Life:	36 months		Confidence:	95 %

CAS #	Certified Component	Requested Concentration	Concentration and Uncertainty	Date of Certification
74-82-8	Methane	30	31.9 +/- 0.3 ppm	01/12/2006
7727-37-9	Nitrogen		Balance	01/12/2006

CAS #	Reference Standard	Cylinder/Standard #	Concentration	Expire Date
74-82-8	Methane	CC24916 , GMIS	50.23 ppm	07/14/2007
74-82-8	Methane	CC156744 , GMIS	10.03 ppm	04/21/2006

Instrument	Serial #	Analytical Principle	Calibration Date
Horiba FIA-510	56847471	Flame Ionization	01/10/2006

All analyses are performed under controlled environmental conditions. This product is manufactured using equipment which has been calibrated with NIST traceable, or equivalent, standards, weights, or equipment.

Analytical report approved by Roy Yoder

Roy Yoder

Analysis Certificate

Facility: Master Location: Fort Smith AR
 Source ID: SN-12 Test Date: 4-17-07

Analyzer Calibration Error

Component	Cylinder No.	Actual Conc.	Analyzer Response	Difference
CO - High				
CO - Mid				
CO - Low				
CO - Zero	-	0.0		0.0
NOx - High				
NOx - Mid				
NOx - Zero	-	0.0		0.0
O ₂ - High		20.9		
O ₂ - Mid				
O ₂ - Zero	-	0.0		0.0
SO ₂ - High				
SO ₂ - Mid				
SO ₂ - Zero	-	0.0		0.0
VOC - High		46	86.3	
VOC - Mid		50.1	49.7	
VOC - Low		31.9	31.6	
VOC - Zero	-	0.0	0.0	0.0

System Calibration Bias

Calibration Gas	Analyzer Response	System Response	Difference
CO - Zero Gas			
CO - Upscale Gas			
NOx - Zero Gas			
NOx - Upscale Gas			
O ₂ - Zero Gas			
O ₂ - Upscale Gas			
SO ₂ - Zero Gas			
SO ₂ - Upscale Gas			
VOC - Zero Gas	0.0	0.1	
VOC - Upscale Gas	31.6	31.4	

System Calibration Drift

Source: SN-12					Date: 4-17-07 → 4-18-07				
Run # 1		Time: 905-1005			Run #		Time: CH4 1010-1020		
Type	Pre-test Value		Post-test Value		Type	Pre-test Value		Post-test Value	
	Zero	Span	Zero	Span		Zero	Span	Zero	Span
CO					CO	THC = 11.9		ppm → 12.0	
NOx					CH4 CH4 = 12.2		ppm		
O2					O2				
SO2					SO2				
VOC	0.1	31.4	-0.4	32.3	VOC				
Run # 2		Time: 1400-1500			Run #		Time: CH4 1510-1520		
Type	Pre-test Value		Post-test Value		Type	Pre-test Value		Post-test Value	
	Zero	Span	Zero	Span		Zero	Span	Zero	Span
CO					CO				
NOx					NOx	THC = 9.8			
O2					O2	CH4 = 9.4			
SO2					SO2				
VOC	0.5	32.6	0.2	31.8	VOC				
Run # 3		Time: 930-1030			Run #		Time: CH4 1040-1050		
Type	Pre-test Value		Post-test Value		Type	Pre-test Value		Post-test Value	
	Zero	Span	Zero	Span		Zero	Span	Zero	Span
CO					CO				
NOx					NOx	THC = 10.7			
O2					O2	CH4 = 10.6			
SO2					SO2				
VOC	0.4	32.0	1.1	33.2	VOC				
Run #		Time:			Run #		Time:		
Type	Pre-test Value		Post-test Value		Type	Pre-test Value		Post-test Value	
	Zero	Span	Zero	Span		Zero	Span	Zero	Span
CO					CO				
NOx					NOx				
O2					O2				
SO2					SO2				
VOC					VOC				
Run #		Time:			Run #		Time:		
Type	Pre-test Value		Post-test Value		Type	Pre-test Value		Post-test Value	
	Zero	Span	Zero	Span		Zero	Span	Zero	Span
CO					CO				
NOx					NOx				
O2					O2				
SO2					SO2				
VOC					VOC				
Run #		Time:			Run #		Time:		
Type	Pre-test Value		Post-test Value		Type	Pre-test Value		Post-test Value	
	Zero	Span	Zero	Span		Zero	Span	Zero	Span
CO					CO				
NOx					NOx				
O2					O2				
SO2					SO2				
VOC					VOC				

System Calibration Drift

Source: SN-01					Date: 4-19-07 → 4-20-07				
Run #	Time: 1130-1230				Run #	Time: CH ₄ = 1240-1250			
Type	Pre-test Value		Post-test Value		Type	Pre-test Value		Post-test Value	
	Zero	Span	Zero	Span		Zero	Span	Zero	Span
CO					CO				
NOx					NOx	THC = 7.6			
O ₂					O ₂	CH ₄ = 7.4			
SO ₂					SO ₂				
VOC	0.4	31.9	0.0	31.4	VOC				
Run #	Time: 1430-1530				Run #	Time: CH ₄ = 1540-1550			
Type	Pre-test Value		Post-test Value		Type	Pre-test Value		Post-test Value	
	Zero	Span	Zero	Span		Zero	Span	Zero	Span
CO					CO				
NOx					NOx	THC = 7.8			
O ₂					O ₂	CH ₄ = 7.2			
SO ₂					SO ₂				
VOC	0.5	32.1	0.1	31.7	VOC				
Run #	Time: 915-1015				Run #	Time: CH ₄ = 1020-1030			
Type	Pre-test Value		Post-test Value		Type	Pre-test Value		Post-test Value	
	Zero	Span	Zero	Span		Zero	Span	Zero	Span
CO					CO				
NOx					NOx	THC = 9.7			
O ₂					O ₂	CH ₄ = 9.6			
SO ₂					SO ₂				
VOC	0.3	31.9	0.6	32.3	VOC				
Run #	Time:				Run #	Time:			
Type	Pre-test Value		Post-test Value		Type	Pre-test Value		Post-test Value	
	Zero	Span	Zero	Span		Zero	Span	Zero	Span
CO					CO				
NOx					NOx				
O ₂					O ₂				
SO ₂					SO ₂				
VOC					VOC				
Run #	Time:				Run #	Time:			
Type	Pre-test Value		Post-test Value		Type	Pre-test Value		Post-test Value	
	Zero	Span	Zero	Span		Zero	Span	Zero	Span
CO					CO				
NOx					NOx				
O ₂					O ₂				
SO ₂					SO ₂				
VOC					VOC				
Run #	Time:				Run #	Time:			
Type	Pre-test Value		Post-test Value		Type	Pre-test Value		Post-test Value	
	Zero	Span	Zero	Span		Zero	Span	Zero	Span
CO					CO				
NOx					NOx				
O ₂					O ₂				
SO ₂					SO ₂				
VOC					VOC				

Dry Gas Meter Calibration Form

Certification Date: 3/31/2007

Pb (in.Hg): 30

Meter Box I.D: Nutech

Orifice Manometer Setting, dH, in.H ₂ O	Wet Test Meter Volume V _w , ft ³	Dry Gas Meter Volume V _m , ft ³	Temperatures				Time Theta, min.
			Wet Test Meter t _w , F	DGM Inlet t _i , F	DGM Outlet t _o , F	DGM Average t _m , F	
0.5	10.00	10.183	70.0	75.7	71.0	73.3	24.85
1.0	10.00	10.072	70.0	75.7	71.0	73.3	17.70
2.0	10.00	10.011	70.0	75.7	71.0	73.3	13.50
3.0	10.00	9.886	70.0	75.7	71.0	73.3	10.50
3.5	11.00	11.054	70.0	75.7	71.0	73.3	10.70

Orifice Manometer Setting, dH, in.H ₂ O	Calibration Factor, Y	Orifice Pressure Differential, dH@
0.5	0.987	1.726
1.0	0.997	1.751
2.0	1.000	2.037
3.0	1.010	1.849
3.5	0.993	1.851
Average:	0.997	1.843
Standard Deviation	0.009	0.123
Acceptable Value?	YES!	YES!

*Tolerances for individual Y values +/- 0.02 from average.

**Tolerances for individual dH@ values +/- 0.20 from average.

$$Y = \frac{V_w P_b (t_m + 460)}{V_m \left[P_b + \frac{dH}{13.6} (t_w + 460) \right]}$$

$$dH@ = \frac{0.0317 dH}{P_b (t_o + 460)} \left[\frac{(t_w + 460) Theta}{V_w} \right]^2$$