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Background Report Reference

AP-42 Section Number: 12.11

Background Chapter: 2

Reference Number: 31

Title: Report of Particulate/Lead Emissions
Test for Refined Metals Corporation
Secondary Lead Smelter, Beech
Grove, Inc.

Environmental Monitoring
Laboratories

June 1989

38

REPORT OF
PARTICULATE/LEAD EMISSIONS TEST
FOR
REFINED METALS CORPORATION
SECONDARY LEAD SMELTER

Beech Grove, Indiana
June 19 and 20, 1989

INDIANA AIR POLLUTION
CONTROL BUREAU

NEW

Performed By:
Environmental Monitoring Laboratories
Ridgeland, Mississippi

ENVIRONMENTAL MONITORING LABORATORIES, INC.

P.O. Box 655 • 224-B Hwy 51 North
Ridgeland, Mississippi 39157

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July 27, 1989

Subject: Refined Metals Corporation - Beech Grove, Indiana
Particulate/lead emissions test, June 19 and 20, 1989

On June 19 and 20, 1989, Environmental Monitoring Laboratories conducted air emissions tests for Refined Metals Corporation's secondary lead smelter in Beech Grove, Indiana. The tests were performed to determine emissions of lead and particulate matter from three emission points in accordance with requirements of the City of Indianapolis' Air Pollution Control Division.

The three emission points from the smelter activity are the blast furnace metalurgical baghouse (M-1), the blast furnace sanitary baghouse (M-2), and the refinery sanitary baghouse (M-3). The results of the tests are:

Source	Particulate	Lead
M-1	1.493 #/hr	0.635 #/hr
M-2	0.350 #/hr	0.051 #/hr
M-3	0.299 #/hr	0.013 #/hr

The testing project was coordinated by Mr. Bill Freudiger, Vice President of Refined Metals Corporation. On site coordination of the project was provided by Mr. Ron Wiedner, plant manager of Refined Metals' Beech Grove operation. Also on site was Mr. Scott Carrol representing Refined Metals. Mr. Mark Caraher of the City of Indianapolis' Air Pollution Control Division witnessed portions of the tests. Danny Russell of Environmental Monitoring Laboratories was responsible for the collection and analysis of all but the lead samples, and custody of those samples was limited to Mr. Russell. Following their use for determining particulate emissions, the lead samples were shipped by way of Mr. E. F. Williams of E. F. Williams and Associates to Environmental Testing and Consulting, Inc. in Memphis, Tennessee, for analysis.

Following is a report of the test.

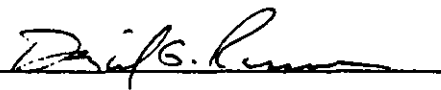
REPORT OF PARTICULATE/LEAD EMISSIONS TESTS
REFINED METALS CORPORATION
BEECH GROVE, INDIANA
JUNE 19 AND 20, 1989

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REPORT CERTIFICATION

I certify that I have examined the information submitted herein, and based upon my inquiries of those directly responsible for obtaining the data or upon my direct acquisition of the data, I believe the submitted information is true, accurate and complete.

Signed 
Daniel G. Russell

1.0 Tests Results: The following tables present the measured flow parameters and test results for emissions tests taken for Refined Metals Corporation in Beech Grove, Indiana during the period June 19 and 20, 1989.

1.1 Refinery Sanitary Baghouse (M-3)

Run. No.		1	2	3	avg.
Date		06-19-89	06-19-89	06-19-89	-----
Time start		1242	1403	1519	-----
Time end		1345	1504	1620	-----
=====					
PARTICULATE EMISSIONS	#/hr.	0.401	0.247	0.247	0.299
PARTICULATE EMISSIONS	gr./dscf	0.003	0.002	0.002	0.002
LEAD EMISSIONS	#/hr.	0.013	0.009	0.016	0.013
VOLUMETRIC FLOWRATE	acfm	20219	18376	18469	19021
VOLUMETRIC FLOWRATE	dscfm	17613	15950	16136	16566
VELOCITY	ft./sec.	64.29	58.43	58.73	60.48
STACK TEMPERATURE	degrees F	123	125	124	124
MOISTURE	%	2.13	2.25	1.69	20.3
SAMPLE RATE	%isokinetic	93	95	93	93
=====					

1.2 Blast Furnace Sanitary Baghouse (M-2)
Particulate/Lead test on June 20, 1989

Run. No.	1	2	3	avg.
Date	06-20-89	06-20-89	06-20-89	-----
Time start	1421	1535	1648	-----
Time end	1523	1637	1749	-----
PARTICULATE EMISSIONS	#/hr.	0.412	0.427	0.211
PARTICULATE EMISSIONS	gr./dscf	0.001	0.001	0.001
LEAD EMISSIONS	#/hr.	0.053	0.055	0.046
VOLUMETRIC FLOWRATE	acfm	39052	38416	37844
VOLUMETRIC FLOWRATE	dscfm	39052	38416	37844
VELOCITY	ft./sec.	45.88	45.13	44.46
STACK TEMPERATURE	degrees F	113	118	111
MOISTURE	%	1.76	1.17	1.90
SAMPLE RATE	%isokinetic	96	97	96

1.3 Blast Furnace Metallurgical Baghouse (M-1)
Particulate/Lead test on June 20, 1989

Run. No.	1	2	3	avg.
Date	06-20-89	06-20-89	06-20-89	-----
Time start	0827	0947	1105	-----
Time end	0929	1049	1207	-----
PARTICULATE EMISSIONS	#/hr.	1.783	1.406	1.291
PARTICULATE EMISSIONS	gr./dscf	0.008	0.007	0.006
LEAD EMISSIONS	#/hr.	0.791	0.657	0.457
VOLUMETRIC FLOWRATE	acfm	29093	28810	28086
VOLUMETRIC FLOWRATE	dscfm	24831	24534	24047
VELOCITY	ft./sec.	40.25	39.85	38.85
STACK TEMPERATURE	degrees F	128	128	123
MOISTURE	%	1.76	1.71	1.90
SAMPLE RATE	%isokinetic	96	97	96

2.0 Source Description: Source operation descriptions and process rates are presented under separate cover. Presented here are descriptions of the sampling locations. In addition to these descriptions, the stacks and selection of sample points are illustrated in the appendix.

2.1 M-1. The blast furnace metalurgical baghouse is equipped with a vertical exhaust stack which is 47.0 inches in diameter and extends about 135 feet above grade. Two sample ports are provided at 90° at a location which is about 100 feet below the stack exit, and 24 feet (6.1 diameters) above the blower inlet duct.

2.2 M-2. The blast furnace sanitary baghouse is equipped with a vertical exhaust stack which is 51.0 inches in diameter and extends about 100 feet above grade. Two sample ports are provided at 90° at a location which is about 46 feet (10.8 diameters) below the stack exit, and 43 feet (10.1 diameters) above the blower inlet duct.

2.3 M-3. The refinery sanitary baghouse is equipped with a vertical exhaust stack which is 32.0 inches in diameter and extends about 80 feet above grade. Two sample ports are provided at 90° at a location which is about 30 feet (11.3 diameters) below the stack exit, and 28 feet (10.5 diameters) above the blower inlet duct.

3.0 Test Procedures: Test procedures used are those described in the Code of Federal Regulations, Title 40, Part 60, Appendix A. Specifically, Method 1 was used to determine the number of sample points, Method 3 to determine excess air and molecular weight of the stack gas, and Methods 5 and 12 to determine flow rates, moisture content, and particulate and lead emissions. Sampling was performed in triplicate. The sampling train used is identical to that described in Method 12. There were no significant departures from the standard procedures.

Particulate adhering to the sample exposed surfaces of the probe and nozzle was washed and brushed with acetone into a sample container. Filters were recovered by rinsing the front half of the filter holder into the probe wash and securing the filters in glass petri dishes. (Some of the filter material usually adheres to the silicone filter gasket and is recovered into the probe wash. Therefore a small amount of the filter weight is usually attributed to the probe wash weight.)

Filters were heated in an oven for 2 hours at 105° C, desiccated at least 24 hours and weighed to constant weight. Probe wash samples in acetone were evaporated to dryness over low heat in tarred beakers, desiccated for at least 24 hours and weighed to constant weight. Weighings were made at 6 hour or longer intervals (samples stored in desiccator). Weights were recorded and considered valid final weights if there was no more than 0.5 milligrams difference from the previous weighing.

Following the particulate analysis, the probe wash residue and filters were combined with the impinger contents residue and prepared for lead analysis in accordance with Method 12.

4.0 Data Reduction

Refined Metals - Refinery Sanitary Baghouse
 Particulate/Lead Emissions Test, June 19, 1989

Collected test data		RUN 1	RUN 2	RUN 3
1. As	: sq ft	5.241442	5.241442	5.241442
2. Dh	: in.	.195	.195	.195
3. Cp	: dimensionless	.84	.84	.84
4. Theta	: minutes	60	60	60
5. Y	: dimensionless	.99	.99	.99
6. Pbar	: in. Hg	29.46	29.46	29.44
7. Pg	: in. H2O	-.5	-.5	-.5
8. Vm	: cf (dry gas)	42.028	38.824	38.711
9. $\text{sqr}(\text{DP}), \text{avg}$	: in. H2O ^{.5}	1.0751	.9757	.9821
10. DH	: in. H2O	1.675	1.3425	1.35
11. ts	: degrees F	123.33	124.75	123.83
12. tm	: degrees F	98.88	99.83	102.79
13. Vlc	: ml	18	17.5	13
14. CO2	: percent	.00	.00	.00
15. O2	: percent	20.50	20.50	20.50
16. Mn	: milligrams	6.7	4.2	4.1
17. M,Pb	: milligrams	.22	.1525	.2625

123.97

Refined Metals - Refinery Sanitary Baghouse
 Particulate/Lead Emissions Test, June 19, 1989

Calculations:	RUN 1	RUN 2	RUN 3	AVG.
1. P_m : in. Hg ($DH/13.6$)+ P_{bar}	29.58	29.56	29.54	N/A
2. P_s : in. Hg ($P_g/13.6$)+ P_{bar}	29.42	29.42	29.40	N/A
3. A_n : sq ft ($(D_n/24)^2$)(3.1416)	2.074e-4	2.074e-4	2.074e-4	N/A
4. V_{mstd} : dscf $V_m Y(P_m/P_{std})(T_{std}/T_m)$	38.86622	35.81271	35.49729	N/A
5. V_{wstd} : scf (.04707cf/ml)(V_{lc})	.84726	.823725	.61191	N/A
6. B_{ws} : dimensionless $V_{wstd}/(V_{wstd}+V_{mstd})$	.0213343	.0224838	.0169461	.0202547
7. M_d : mol.wt. dry basis .44 CO ₂ +.32 O ₂ +.28(CO+N ₂)	28.82	28.82	28.82	N/A
8. M_s : mol.wt. wet basis $M_d(1-B_{ws})+18 B_{ws}$	28.59	28.58	28.64	N/A
9. V_s : ft/sec $K_p C_p (\text{sqr} DP) \text{sqr}(T_s/(P_s M_s))$	64.29	58.43	58.73	60.48
10. Q : cfm $V_s A_s(60 \text{ sec/min})$	20219	18376	18469	19021
11. Q_{std} : dscfm $Q(1-B_{ws})(P_s/P_{std})(T_{std}/T_s)$	17613	15950	16136	16566
12. I : percent [(100 T_s)(.002669 $V_{lc}+(V_m P_m/T_m)$)]/ (60 Theta $V_s P_s A_n$)	92.95	94.58	92.66	93.40
13. E : pounds/hr ((M_n/V_{mstd})(Q_{std})(60))/453590 mg/#	.4016334	.2474361	.2465311	.2985335
14. C/s : grains/dscf (M_n/V_{mstd})(.0154 grains/mg)	.0026547	.0018061	.0017787	.0020798
15. E_{Pb} : pounds/hr ((M_{Pb}/V_{mstd})(Q_{std})(60))/453590	.0131880	.0089843	.0157840	.0126521

Refined Metals - Blast Furnace Sanitary Baghouse
 Particulate/Lead Emissions Test, June 20, 1989

Collected test data	RUN 1	RUN 2	RUN 3
1. As : sq ft	14.18625	14.18625	14.18625
2. Dn : in.	.261	.261	.261
3. Cp : dimensionless	.84	.84	.84
4. Theta : minutes	60	60	60
5. Y : dimensionless	.99	.99	.99
6. Pbar : in. Hg	29.47	29.47	29.48
7. Pg : in. H2O	-.37	-.37	-.37
8. Vm : cf (dry gas)	57.074	56.696	56.124
9. sqn(DP),avg: in.H2O ^{1.5}	.7752	.759	.7535
10. DH : in. H2O	3.0458	2.9333	2.9167
11. ts : degrees F	112.58	118.08	109.00
12. tm : degrees F	103.08	111.00	111.41
13. Vlc : ml	20	19	21
14. CO2 : percent	.00	.00	.00
15. O2 : percent	20.50	20.50	20.50
16. Mn : milligrams	4.7	4.9	2.4
17. M,Pb : milligrams	.6055	.6325	.5175

113.22

Refined Metals - Blast Furnace Sanitary Baghouse
Particulate/Lead Emissions Test, June 20, 1989

Calculations:	RUN 1	RUN 2	RUN 3	AVG.
1. P_m : in. Hg ($DH/13.6$)+ P_{bar}	29.69	29.69	29.69	N/A
2. P_s : in. Hg ($P_g/13.6$)+ P_{bar}	29.44	29.44	29.45	N/A
3. A_n : sq ft $((D_n/24)^2)(3.1416)$	$3.715e-4$	$3.715e-4$	$3.715e-4$	N/A
4. V_{mstd} : dscf $V_m Y(P_m/P_{std})(T_{std}/T_m)$	52.58281	51.49569	50.95465	N/A
5. V_{wstd} : scf $(.04707cf/ml)(V_{lc})$	.9414	.89433	.98847	N/A
6. B_{ws} : dimensionless $V_{wstd}/(V_{wstd}+V_{mstd})$	.0175883	.0170706	.0190299	.0178963
7. M_d : mol.wt. dry basis .44 CO_2 +.32 O_2 +.28($CO+N_2$)	28.82	28.82	28.82	N/A
8. M_s : mol.wt. wet basis $M_d(1-B_{ws})+18 B_{ws}$	28.63	28.64	28.61	N/A
9. V_s : ft/sec $K_p C_p (sqr DP)sqr(T_s/(P_s M_s))$	45.88	45.13	44.46	45.16
10. Q : cfm $V_s A_s(60 \text{ sec/min})$	39052	38416	37844	38437
11. Q_{std} : dscfm $Q(1-B_{ws})(P_s/P_{std})(T_{std}/T_s)$	34814	33939	33911	34221
12. I : percent $[(100 T_s)(.002669 V_{lc}+(V_m P_m/T_m)]/$ $(60 \text{ Theta } V_s P_s A_n)$	96.12	96.56	95.62	96.10
13. E : pounds/hr $((M_n/V_{mstd})(Q_{std})(60))/453590 \text{ mg/\#}$	.4116216	.4271768	.2112795	.3500260
14. $C's$: grains/dscf $(M_n/V_{mstd})(.0154 \text{ grains/mg})$	.0013765	.0014654	.0007254	.0011891
15. E, Pb : pounds/hr $((M, Pb/V_{mstd})(Q_{std})(60))/453590$	.0530291	.0551407	.0455571	.0512423

Refined Metals - Blast Furnace Metallurgical Baghouse
Particulate/Lead Emissions Test, June 20, 1989

Collected test data		RUN 1	RUN 2	RUN 3
1. As	: sq ft	12.04823	12.04823	12.04823
2. Dn	: in.	.261	.261	.261
3. Cp	: dimensionless	.84	.84	.84
4. Theta	: minutes	60	60	60
5. Y	: dimensionless	.99	.99	.99
6. Pbar	: in. Hg	29.47	29.47	29.49
7. Pg	: in. H2O	-.2	-.2	-.2
8. Vm	: cf (dry gas)	48.119	47.122	46.992
9. sqr(DP),avg	: in.H2O ^{.5}	.6705	.6639	.6498
10. DH	: in. H2O	2.27	2.2125	2.0825
11. ts	: degrees F	128.25	127.70	122.55
12. tm	: degrees F	89.80	96.25	101.40
13. Vlc	: ml	34	36	39.5
14. CO2	: percent	1.00	1.00	1.00
15. O2	: percent	20.00	20.00	20.00
16. Mn	: milligrams	24.6	19	17.6
17. M,Pb	: milligrams	10.9075	8.8775	6.2275

126.17

Refined Metals - Blast Furnace Metallurgical Baghouse
Particulate/Lead Emissions Test, June 20, 1989

Calculations:	RUN 1	RUN 2	RUN 3	AVG.
1. Pm : in.Hg (DH/13.6)+Pbar	29.64	29.63	29.64	N/A
2. Ps : in. Hg (Pg/13.6)+Pbar	29.46	29.46	29.48	N/A
3. An : sq ft ((Dn/24)^2)(3.1416)	3.715e-4	3.715e-4	3.715e-4	N/A
4. Vmstd: dscf Vm Y(Pm/Pstd)(Tstd/Tm)	45.31608	43.85632	43.34939	N/A
5. Vwstd: scf (.04707cf/m)(Vlc)	1.60038	1.69452	1.859265	N/A
6. Bws : dimensionless Vwstd/(Vwstd+Vmstd)	.0341113	.0372006	.0411263	.0374794
7. Md : mol.wt. dry basis .44 CO2+.32 O2+.28(CO+N2)	28.96	28.96	28.96	N/A
8. Ms : mol.wt. wet basis Md(1-Bws)+18 Bws	28.59	28.55	28.51	N/A
9. Vs : ft/sec Kp Cp (sqrDP)sqr(Ts/(Ps Ms))	40.25	39.85	38.85	39.65
10. Q : cfm Vs As(60 sec/min)	29093	28810	28086	28663
11. Qstd : dscfm Q(1-Bws)(Ps/Pstd)(Tstd/Ts)	24831	24534	24047	24470
12. I : percent [(100 Ts)(.002669 Vlc+(Vm Pm/Tm)]/ (60 Theta Vs Ps An)	98.64	96.61	97.43	97.56
13. E : pounds/hr ((Mn/Vmstd)(Qstd)(60))/453590 mg/#	1.783038	1.405958	1.291425	1.493474
14. C's : grains/dscf (Mn/Vmstd)(.0154 grains/mg)	.0083599	.0066718	.0062525	.0070947
15. E,Pb : pounds/hr ((M,Pb/Vmstd)(Qstd)(60))/453590	.7905890	.6569154	.4569518	.6348188

5.0 NOMENCLATURE

SYMBOL	UNITS	DESCRIPTION
An	ft ²	Nozzle area
As	ft ²	Stack area
B _{us}	dimensionless	Proportion of water vapor
CO ₂	percent	Carbon dioxide content by volume
CO	percent	Carbon monoxide content by volume
C _p	dimensionless	Pitot correction factor
C's	grains/dscf	Particulate concentration
C,SO ₂	ppm	Sulfur dioxide concentration
D _n	inches	Nozzle diameter
delta H	in. H ₂ O	Pressure drop across meter orifice (also DH)
delta P	in. H ₂ O	Stack velocity pressure head (also DP)
E	#/hr	Particulate emission rate
E,lead	#/hr	Lead emission rate
E,SO ₂	#/hr	Sulfur dioxide emission rate
I	percent	Percent isokinetic sampling
K _p	consistent	Pitot tube constant = 85.49
M _n	milligrams	Particulate sample weight
M _d	#/mole	Dry molecular wt. of stack gas
M _s	#/mole	Wet molecular wt. of stack gas
N ₂	percent	Nitrogen content by volume
O ₂	percent	Oxygen content by volume
P _{bar}	in. Hg	Barometric pressure
P _g	in. H ₂ O	Static pressure
P _m	in. Hg	Meter pressure = P _{bar} + (delta H/13.6)
P _s	in. Hg	Stack pressure = P _{bar} + (P _g /13.6)
P _{std}	in. Hg	Standard pressure = 29.92
Q	ft ³ /min	Volumetric flow rate at stack conditions
Q _{std}	dscf/min	Volumetric flow rate at dry, std. conditions
Theta	minutes	Sampling time per run
t _m	°F	Meter temperature (T _m denotes °R)
t _s	°F	Stack temperature (T _s denotes °R)
T _{std}	°R	Standard temperature = 528°
V _{lc}	ml	Volume of water collected
V _m	ft ³	Volume of dry gas sampled
V _{mstd}	dscf	Sample volume at standard conditions
V _{wstd}	scf	Sample volume of water vapor
Y	dimensionless	Meter correction factor

6.0 Calibrations:

Measurement devices used by Environmental Monitoring Laboratories and subject to changes in measurement precision are initially calibrated prior to use. Those instruments for which calibration factors are subject to change or for which calibration checks are required, are calibrated following each field use or as otherwise directed and noted. Calibration procedures for specific equipment are as follows.

Dry Gas Meter:

Dry gas meters are periodically removed from the sampling consoles and cleaned and repaired (new gaskets etc. as required). Following the overhaul of a meter, the measuring precision is checked by the Bell Prover Method and adjusted when necessary to read to within 2% of 100% accuracy. This service is provided by Big Three Meter Company in Jackson, Mississippi. Overhaul service or any six month period is followed by a five point calibration described in APTD-0576 using either a wet test meter or calibrated dry gas meter (used exclusively for calibrations) as a standard reference. Following field use, a gas meter calibration is checked in one of two ways. [1] Three calibration checks at intermediate orifice settings are performed or [2] orifice meter coefficients are used.

If a meter coefficient obtained from pre-test and post-test checks differs by more than 5%, the coefficient (Y) giving the lower sample volume is used in the calculations.

Orifice:

The orifice coefficient is initially determined and is rechecked following a major gas meter repair and calibration.

Nozzles:

Nozzles are checked before each field use with a precision (.001 in.) dial caliper. Three measurements on different axes are made; an average of those three readings is used in calculations. If the tolerance among measurements exceeds 0.004 inches (highest to lowest reading) the nozzle is repaired and recalibrated or discarded.

Pitot Tubes:

Pitot tubes meeting EPA geometry standards are assigned a coefficient of 0.84. Pitot tubes are visually inspected for damage before, during and after use. Those pitot tubes not meeting the geometry standards are assigned a coefficient from the manufacturer's calibration which it retains unless damaged. All pitot tubes used by Environmental Monitoring Laboratories are manufactured by NAPP, Inc.

Temperature Measuring Instruments:

Most temperature measurements are made with a type K thermocouple and an Omega digital thermocouple thermometer which has an initial calibration traceable to NBS. Other measurements are made using bimetallic dial thermometers. The thermocouples and dial thermometers are checked following or during a test series against an ASTM mercury in glass thermometer.

Barometer:

Aneroid field barometers are checked against and adjusted to readings from a mercury barometer or readings obtained from local weather authorities.

Differential Pressure Gauges:

Velocity head (ΔP) and orifice pressure differential (ΔH) measurements are made using water manometers of the appropriate range unless otherwise noted in the test data. Manometers do not require calibration.

- 7.0 Appendices
 - a. Test Data
 - b. Calibration Data

SAMPLING AND PARTICULATE ANALYSIS DATA

REFINERY SANITARY BAGHOUSE (M-3)

STACK CONFIGURATION / SAMPLE AND VELOCITY POINTS

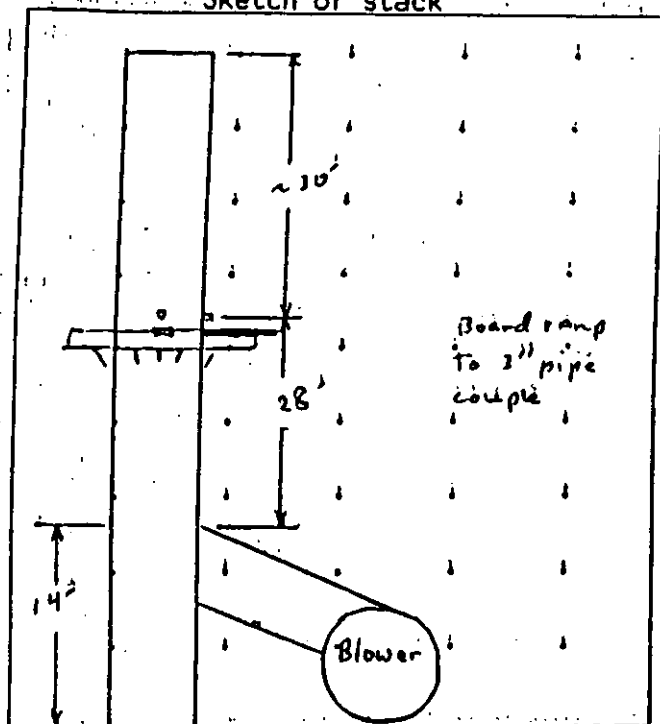
Plant Name Refined Metals - Indianapolis

Source Refinery Sanitary Bayshore

Date For: Particulate Preliminary Process

Date 11-17-87

Sketch of stack



%Diameter

	4	6	8	10	12	14	16
1	6.7	4.4	3.2	2.6	2.1	1.8	1.6
2	25.0	14.6	10.5	8.2	6.7	5.7	4.9
3	75.0	29.6	19.4	14.6	11.8	9.9	8.5
4	93.3	70.4	32.3	22.6	17.7	14.6	12.5
5		85.4	67.7	34.2	25.0	20.1	16.9
6		95.6	80.6	65.8	35.6	26.9	22.0
7			89.5	77.4	64.4	36.6	28.3
8			96.8	85.4	75.0	63.4	37.5
9				91.8	82.3	73.1	62.5
10				97.4	88.2	79.9	71.7
11					93.3	85.4	78.0
12					97.9	90.1	83.1
13						94.3	87.5
14						98.2	91.5
15							95.1
16							98.4

Velocity profile / Sample point layout

pitot I.D. 2.06

pitot Cp .84

pg 6455

ts: 90

Point No.	"from wall	delta P
1	1.4	1.40
2	4.7	1.60
3	9.5	1.90
4	22.5	2.00
5	27.3	1.90
6	30.6	1.85
7		
8		
9		
10		
11		
12		
13		
14		
15		
16		

Stack diameter 32.0

Distance from ports to disturbance:

distance to upstream disturbance ~28

distance to downstream disturbance ~30

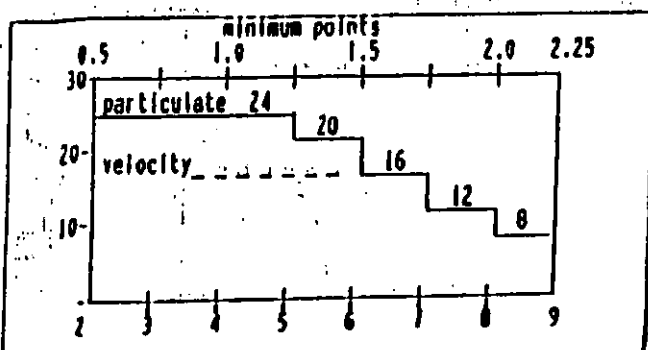
upstream diameters 10.5

downstream diameters 11.3

Minimum No. points required 12

No. points selected 12

Nipple length 3.5"



Notes:

Scott Campbell CO

RUN No. 2
Date 6-19-89
Time start 1403 and 1504

Remarks:

Condensate:
tare 220.4402 fin 211
Silica gel:
tare 702.5 fin 709

[illegible]

Plant Refined Metals
 Sampling Location Refining Section Baghouse
 Test For Particulate / Lead
 Test Operators Russell / Turner

RUN No. 3
 Date 6-15-89
 Time start 1515 end 1620

Meter Box RAC 59329
 Sample Box No. 2
 Probe/Pitot 2' Qc
 Pitot Cp .87
 Nozzle Dia. .195
 Filter No.

No. Sample Pts. 6x2
 Minutes/Pt. 5
 NOMOGRAPH
 $\Delta H @$ 1.95
 Meter Temp. 100
 % H₂O 8
 C-Factor 1.05
 Stack Temp. 130
 Ref. ΔP 1.3

Gas Analysis Fytr
 CO₂ 0
 O₂
 CO
 Time
 Condensate:
 tare 200 H₂O in 207
 Silica gel:
 tare 863 in 669

Remarks:

Amb. Temp. °F 84
 Bar. Press. "Hg 29.44
 Static Press. "H₂O -.50

Port Point	El. Time, Min.	OGM Reading, Ft.	Velocity Head ΔP , in. H ₂ O	Orifice ΔH in. H ₂ O	Stack Temp. °F	Meter Temp., °F In Out	Oven Temp. °F	Imp. Temp. °F	Vac in. Hg
1	0	845.811	0.92	1.30	124	96 96	200	67	3
2	5	849.3	0.93	1.30	125	102 98	210	65	3
3	10	852.2	1.00	1.40	126	104 98	220	64	2
4	15	855.5	1.00	1.40	128	105 99	225	60	2
5	20	858.6	0.90	1.25	125	107 100	250	66	2
6	25	861.8	0.82	1.15	124	108 100	245	65	2
1	30/0	864.2856	1.00	1.40	127	105 100	250	64	2
2	5	868.3	1.10	1.50	120	104 98	225	68	2
3	10	871.5	1.20	1.70	124	107 100	220	65	2
4	15	875.2	1.10	1.50	123	110 100	210	65	2
5	20	878.5	0.90	1.25	121	113 102	220	65	2
6	25	881.7	0.75	1.05	122	111 104	225	65	2
and	60	887.522							
back check: 072 → 073 = 001 ΔH 7" ΔH									
pitot + v = 5.9 pitot + v = 6.9									
38	71	9821	1350	123.83	104.79				

R. Metals

PARTICULATE CATCH ANALYSIS:

SAMPLES: Refinery Sanitary Baghouse
 DATE TAKEN: 6-19 DATE ANALYZED: 6-22
 SAMPLES DELIVERED BY: DGA RECEIVED BY: DGA
 ANALYZED BY: DGR

Filter treatment: Filters oven dried 2 hours at 105° C, desiccated at least 24 hours, weighed to constant weight

FILTERS:	Run 1	Run 2	Run 3
Filter No.	4042	4040	4041
Tare wt., g	4252	4277	4319
	4223	4232	4288
	4223	4232	4286
Final wt., g	4223	4232	4286
Net gain, g	0.0029	0.0045	0.0033

Probe wash treatment: Transferred to tared beaker, acetone evaporated over low heat, desiccated at least 24 hours, weighed to constant weight.

PROBE WASH:	Run 1	Run 2	Run 3	Blank
Container ID	RMRSBR1	RMRSBR2	RMRSBR3	
Volume Intact?	✓	✓	✓	
Volume, ml	120	145	125	200
Tare wt., g	(1) 103.2059	(2) 98.8552	(22) 99.0948	
	102.455	98.8651	99.1025	
	103.2158	98.8647	99.1025	
Final wt., g	103.2158	98.8647	99.1025	
Net gain, g	0.0099	0.0091	0.0077	0.0005
Less blank, g	-0.0003	-0.0004	-0.0003	

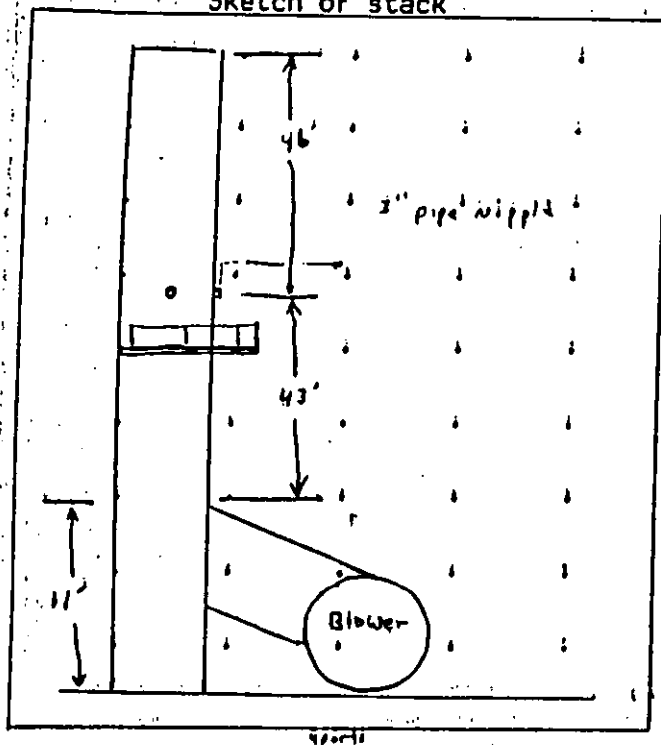
PARTICULATE	Run 1	Run 2	Run 3
Filter+probe	6.7	4.2	4.1

BLAST FURNACE SANITARY BAGHOUSE (M-2)

STACK CONFIGURATION / SAMPLE AND VELOCITY POINTS

Plant Name Refined Metals - Indianapolis Source Blow Furnace - Sintering Bedhouse
 Data For: Preliminary Velocity Date 11-16-87

Sketch of stack



%Diameter

	4	6	8	10	12	14	16
1	6.7	4.4	3.2	2.6	2.1	1.8	1.6
2	25.0	14.6	10.5	8.2	6.7	5.7	4.9
3	75.0	29.6	19.4	14.6	11.8	9.9	8.5
4	93.3	70.4	32.3	22.6	17.7	14.6	12.5
5		85.4	67.7	34.2	25.0	20.1	16.9
6		95.6	80.6	65.8	35.6	26.9	22.0
7			89.5	77.4	64.4	36.6	28.3
8			96.8	85.4	75.0	63.4	37.5
9				91.8	82.3	73.1	62.5
10				97.4	88.2	79.9	71.7
11					93.3	85.4	78.0
12					97.9	90.1	83.1
13						94.3	87.5
14						98.2	91.5
15							95.1
16							98.4

Velocity profile / Sample point layout

pitot 1:0.5
 pitot Cp 84

pg 2 of 2

Point No.	"From wall	delta P
1	2.2	1.40
2	7.4	1.45
3	15.1	1.46
4	35.9	1.44
5	43.6	1.42
6	48.8	1.39
7		
8		
9		
10		
11		
12		
13		
14		
15		
16		

Stack diameter 51.0"

Distance from ports to disturbance:

distance to upstream disturbance 43'

distance to downstream disturbance 46'

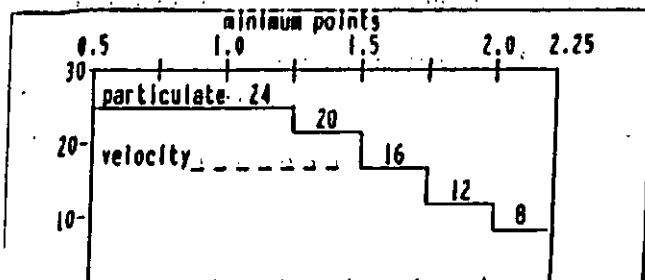
upstream diameters 10.1

downstream diameters 10.8

Minimum No. points required 12

No. points selected 12

Nipple length 3" pn 4"



Notes:

Plant Refined Metals - Beach Grove, Indiana
 Sampling Location Plant Effluent Sanitary Baghouse
 Test For Particulate / Lead
 Test Operators Russell / Tanner

RUN No. 1
 Date 6-20-89
 Time start 1421 end 1523

Meter Box RACS91299
 Sample Box No. 1
 Probe/Pitot 4' OG
 Pitot Cp .87
 Nozzle Dia. .261
 Filter No. 294

No. Sample Pts. 6x2
 Minutes/Pt. 5
 NOMOGRAPH
 $\Delta H @$ 1.95
 Meter Temp. 95
 % H₂O 8
 C-Factor 1.1
 Stack Temp. 110
 Ref. ΔP .31

Gas Analysis Exite
 CO, 0
 O, 20.5
 CO
 Time
 Condensate:
 tare 200 HNO₃ fln 607
 Silica gel:
 tare 716 fln 729

Remarks:

Amb. Temp. °F 88
 Bar. Press. "Hg 29.42
 Static Press. "H₂O -3.7

Port Point	El. Time, Min.	DGM Reading, Ft. ³	Velocity Head ΔP , in. H ₂ O	Orifice ΔH , in. H ₂ O	Stack Temp. °F	Meter Temp., °F In Out	Oven Temp. °F	Imp. Temp. °F	Vac in. Hg
E 1	0	0.271	0.60	3.00	112	96 90	240	70	3
2	5	0.32	0.61	3.10	110	98 91	225	65	2
3	10	0.37	0.60	3.00	114	108 96	240	65	3
4	15	0.42	0.64	3.30	115	107 93	240	65	3
5	20	0.46	0.56	2.85	115	110 95	240	65	2
6	25	0.51	0.51	2.60	113	111 95	240	65	2
N 1	20/0	0.55	0.72	3.70	112	110 98	250	65	3
2	15	0.61	0.71	3.70	113	114 99	255	60	3
3	10	0.66	0.70	3.60	113	117 102	250	62	3
4	15	0.71	0.59	2.90	111	117 99	250	65	3
5	20	0.76	0.52	2.60	111	120 98	250	66	2
6	25	0.80	0.48	2.20	111	115 101	250	67	2
and 60		0.84							
leak check: 0.85 → 0.99 = 0.094 ft ³ 6" H ₂ O pitot - 6.3 pitot - 3.2									
		57.974	7752	3.0198	112.58	103.0			

RUN No. 2
Date 6-20-89
Time start 1535 end 1637

Remarks:

Condensate:
tare 200 HNO₃ fln 206
Silica gel:
tare 669 fln 681

[illegible]

R. Metals

PARTICULATE CATCH ANALYSIS

SAMPLES: Blast Furnace Sanitary Bayhouse
 DATE TAKEN: 6-20-81 DATE ANALYZED: 6-22-81
 SAMPLES DELIVERED BY: DEB RECEIVED BY: _____
 ANALYZED BY: DEB

Filter treatment: Filters oven dried 2 hours at 105° C, desiccated at least 24 hours, weighed to constant weight

FILTERS:	RUN 1	Run 2	Run 3
Filter No.	4031	4032	4046
Tare wt., g	4259	4267	4200
	1188	4209	4178
	4188	4209	4176
Final wt., g	4188	4209	4176
Net gain, g	-0071	-0058	-0024

Probe wash treatment: Transferred to tared beaker, acetone evaporated over low heat, desiccated at least 24 hours, weighed to constant weight.

PROBE WASH:	Run 1	Run 2	Run 3	Blank
Container ID				
Volume intact?				
Volume, ml	130	150	150	200
Tare wt., g	(29) 98.3196	(31) 95.7726	(32) 97.5795	109.6529
	98.4120	95.7838	97.5848	
	98.4117	95.7837	97.5847	
Final wt., g	98.4117	95.7837	97.5847	109.6534
Net gain, g	.0121	.0111	.0052	.0005
Less blank, g	-0003	-0004	-0004	

PARTICULATE	Run 1	Run 2	Run 3
Filter+probe	4.7	4.9	2.4

BLAST FURNACE METALURGICAL BAGHOUSE (M-1)

STACK CONFIGURATION / SAMPLE AND VELOCITY POINTS

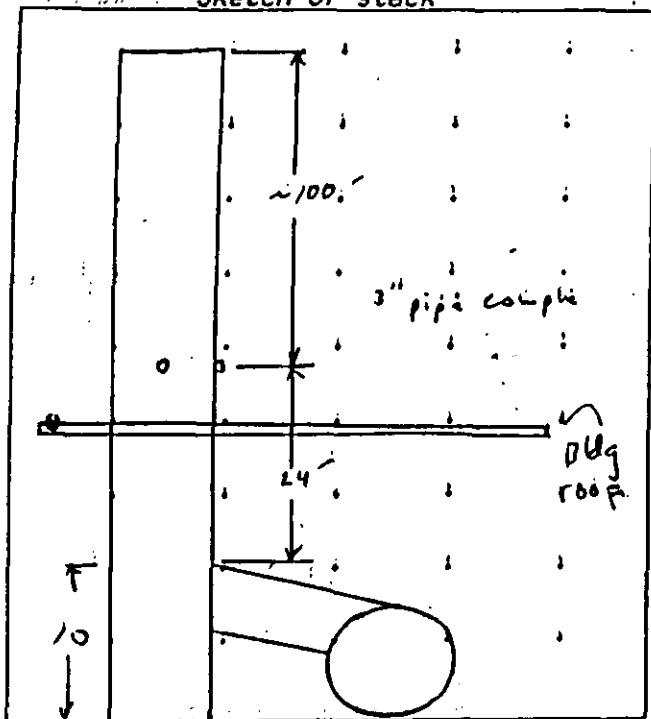
Plant Name Refined Metals

Source Blast Furnace Metallurgical Bldg

Data For: Particulate Velocity

Date 11-17-87

Sketch of stack



%Diameter

	4	6	8	10	12	14	16
1	6.7	4.4	3.2	2.6	2.1	1.8	1.6
2	25.0	14.6	10.5	8.2	6.7	5.7	4.9
3	75.0	29.6	19.4	14.6	11.8	9.9	8.5
4	93.3	70.4	32.3	22.6	17.7	14.6	12.5
5		85.4	67.7	34.2	25.0	20.1	16.9
6		95.6	80.6	65.8	35.6	26.9	22.0
7			89.5	77.4	64.4	36.6	28.3
8			96.8	85.4	75.0	63.4	31.5
9				91.8	82.3	73.1	62.5
10				97.4	88.2	79.9	71.7
11					93.3	85.4	78.0
12					97.9	90.1	83.1
13						94.3	87.5
14						98.2	91.5
15							95.1
16							98.4

Velocity profile / Sample point layout

pitot I.D. 5.9

pitot C_p 1.2

Point No.	"from wall	delta P
1	1.2	1.25
2	3.1	1.20
3	6.9	1.50
4	10.6	1.50
5	16.1	1.5
6	20.9	1.1
7	36.4	1.2
8	40.1	1.2
9	43.1	1.1
10	48.3	1.2
11		
12		
13		
14		
15		
16		

Stack diameter 47.0

Distance from ports to disturbance:

distance to upstream disturbance 24"

distance to downstream disturbance ~100'

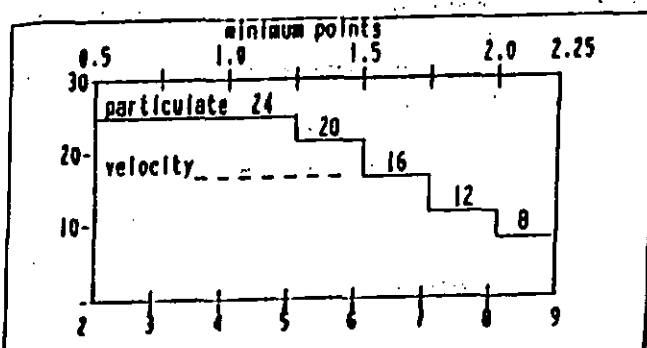
upstream diameters 6.1

downstream diameters >20

Minimum No. points required 16

No. points selected 20

Nipple length 4"



Notes:

Plant <u>Refined Metals - Beach Game, Indiana</u>		RUN No. <u>2</u>	
Sampling Location <u>Plant Entrance Bay Area</u>		Date <u>6-20-59</u>	
Test For <u>Particulate / Lead</u>		Time start <u>0947</u> end <u>1049</u>	
Test Operators <u>Russell / Tanner</u>			

Meter Box	<u>RACS9144</u>	No. Sample Pts.	<u>10 x 2</u>	Gas Analysis	<u>Exhaust</u>	Remarks:
Sample Box	<u>No 2</u>	Minutes/Pl.	<u>3.0</u>	CO,	<u>1.0</u>	
Probe/Pilot	<u>4' AG</u>	NOMOGRAPH $\Delta H @$ <u>1.95</u> Meter Temp. <u>95</u> % H ₂ O <u>8</u> C-Factor <u>1.05</u> Stack Temp. <u>130</u> Ref. ΔP <u>0.37</u>	O,	<u>20.0</u>		
Pilot Cp	<u>.84</u>		CO			
Nozzle Dia.	<u>.261</u>		Time			
Filter No.			Condensate:			
			tare <u>200</u>	fin <u>221</u>		
Amb. Temp. °F	<u>79</u>	Silica gel:				
Bar. Press. "Hg	<u>29.77</u>	tare <u>613</u>	fin <u>620</u>			
Static Press. "H ₂ O	<u>-1.20</u>					

[illegible]

Plant Refined Petrol - Beach GroveSampling Location Point Furman Metallurgical RefineryTest For Particulate / LeadTest Operators Russell / TersonRUN No. 3Date 6-20-89Time start 1105 end 1207Meter Box RAC57145Sample Box 10.3Probe/Pitot 4' probePitot Cp .84Nozzle Dia. .261

Filter No. _____

No. Sample Pts. 10 x 2Minutes/Pt. 3

NOMOGRAPH

 $\Delta H @$ 1.95Meter Temp. 95% H₂O 8C-Factor 1.05Stack Temp. 120Ref. ΔP .27Gas Analysis EgiteCO₂ 1.0O₂ 20.0

CO _____

Time _____

Condensate:

tare 200 H₂O fin 229

Silica gel:

tare 703.5 fin 719

Remarks: _____

Port Point	El. Time, Min.	DGM Reading, Ft.	Velocity Head ΔP , in. H ₂ O	Orifice ΔH , in. H ₂ O	Stack Temp., °F	Meter Temp., °F In Out	Oven Temp., °F	Imp. Temp., °F	Vac In. Hg
E 1	0	98.0, 41.0	0.40	2.00	126	91 91	185	66	2
2	3	98.2, 9	0.38	1.85	122	95 91	215	65	2
3	6	98.5, 2	0.41	2.00	124	102 93	225	63	2
4	9	98.7, 3	0.42	2.00	122	102 93	220	62	2
5	12	98.9, 5	0.45	2.20	120	102 92	225	60	3
6	15	99.1, 7	0.47	2.30	124	106 95	225	60	3
7	18	99.4, 3	0.50	2.45	125	110 95	230	60	3
8	21	99.6, 7	0.47	2.30	122	108 95	225	60	3
9	24	99.9, 5	0.47	2.30	121	107 95	225	60	3
10	27	001, 7	0.39	1.95	120	110 95	235	60	2
S 1	30/0	003, 9.8.3	0.48	2.40	123	106 95	240	61	3
2	3	006, 8	0.47	2.30	121	108 98	240	60	3
3	6	009, 6	0.50	2.45	121	108 96	220	60	3
4	9	011, 6	0.53	2.65	126	111 98	220	60	3
5	12	014, 2	0.47	2.30	126	112 99	220	60	3
6	15	016, 8	0.40	1.95	122	111 99	225	61	2
7	18	019, 0	0.38	1.85	125	113 100	220	63	2
8	21	021, 5	0.32	1.55	121	112 101	240	65	2
9	24	023, 8	0.31	1.50	120	111 100	235	65	2
10	27	025, 3	0.28	1.35	120	111 101	235	65	2
nd 60		027, 40.2							

back back: 050 → 055 = 005 g.p.e 6" H₂O
 pitot at 7.0
 pitot at 8.0

46.992

.6498

2.0825

122.55

101.40

Refined Metals

PARTICULATE CATCH ANALYSIS

SAMPLES: Blast Furnace Metallurgical Baghouse
 DATE TAKEN: 6-20-89 DATE ANALYZED: 6-22-89
 SAMPLES DELIVERED BY: DGR RECEIVED BY: DGR
 ANALYZED BY: DGR

Filter treatment: Filters oven dried 2 hours at 105° C, desiccated at least 24 hours, weighed to constant weight

FILTERS:	Run 1	Run 2	Run 3
Filter No.	4043	4045	4047
Tare wt., g	.4249	.4199	.4376
	.4277	.4243	.4378
	.4276	.4242	.4377
Final wt., g	.4276	.4242	.4377
Net gain, g	.0027	.0043	.0001

Probe wash treatment: Transferred to tared beaker, acetone evaporated over low heat, desiccated at least 24 hours, weighed to constant weight.

PROBE WASH:	Run 1	Run 2	Run 3	Blank
Container ID	RMBMB.R1	RMBMB.R2	RMBMB.R3	
Volume intact?				
Volume, ml	240	255	270	200
Tare wt., g	(23) 96.6339	(25) 97.0951	(26) 98.6879	
	96.6668	97.1109	98.7062	
	96.6564	97.1111	98.7060	
Final wt., g	96.6564	97.1111	98.7060	
Net gain, g	.0225	.0153	.0182	.0005
Less blank, g	-.0006	-.0006	-.0007	

PARTICULATE	Run 1	Run 2	Run 3
Filter+probe	24.6	19.0	17.6

LEAD ANALYSIS REPORT



ENVIRONMENTAL TESTING & CONSULTING INC.

2924 WALNUT GROVE RD. • MEMPHIS, TENN 38111 • PHONE (901) 327-2750

July 24, 1989

Mr. Edward F. Williams III, P.E.
E.F. Williams & Associates, Inc.
3637 Park Ave., Suite 224
Memphis, TN 38111

REF: ANALYTICAL TESTING
SAMPLE DATE: JUNE 1989 STACK TESTS
REFINED METALS, BEECH GROVE, INDIANA
P.O. 02304

Dear Mr. Williams:

The above referenced samples have been analyzed per your instructions. The tests were performed in our laboratory (#00210) in accordance with EPA Method 12. The results are shown below:

<u>Sample I.D.</u>	<u>Lead Results (mg/sample)</u>	<u>By</u>	<u>Date</u>	
001	0.3425	JF	6/29	RSB
002	0.275	JF	6/29	
003	0.385	JF	6/29	
004	11.03	JF	6/29	MB
005	9.00	JF	6/29	
006	6.35	JF	6/29	
007	0.728	JF	6/29	MSB
008	0.755	JF	6/29	
009	0.640	JF	6/29	
010	12.7	JF	6/29	IN
011	7.85	JF	6/29	
012	14.3	JF	6/29	
013	5.70	JF	6/29	Perf
014	4.83	JF	6/29	
015	4.60	JF	6/29	
016	0.113	JF	6/29	BLANKS
017	0.078	JF	6/29	
018	0.027	JF	6/29	

If you have any questions please call me.

Very truly yours,

Michael J. Cimballo
President

MJC/mg

Blank = .1225 mg

CHAIN OF CUSTODY RECORD FOR SAMPLES

PROJECT DESCRIPTION: Plants: Refined Metals - Indianapolis Date: 6-20-89
Tests on Refinery Baghouse, Blast Furnace Metallurgical Baghouse, Blast
Furnace Metallurgical Baghouse, for particulate and lead emissions on
June 19 + 20, 1989

SAMPLE DESCRIPTION:

Sample Container ID

Sample Description:

001 RMRSBR1
 002 RMRSBR2
 003 RMRSBR3
 004 RMBFMBR1
 005 RMBFMBR2
 006 RMBFMBR3
 007 RMBFSBR1
 008 RMBFSBR2
 009 RMBFSBR3
 016 Filter Blank No. 1
 017 Filter Blank No. 2
 018 HNO₃ Blank

SAMPLE COLLECTION:

Collected by: (signature) Daniel G. Rouse
 Date and time of last sample: Afternoon 6-20-89
 Delivered to: EMC - DGR
 Remarks: no custody exchange

SAMPLE RECOVERY:

Recipient of samples for recovery (signature): Daniel G. Rouse
 Recovered by: (signature) Daniel G. Rouse
 Date/time/location of recovery: 6-21-89 EMC - Ridgeland, MS.
 Delivered to: EMC
 Remarks: no custody exchange

SAMPLE ANALYSIS:

Recipient of samples for analysis (signature): _____
 Samples analyzed by (signature): _____

Date/time/location of analysis: _____
 Remarks: _____

SAMPLE CUSTODY TRANSFER:

No.	From/To	Relinquished by	Accepted by	Date/Time
1	EMC/E.F. Williams	Daniel G. Rouse	E.F. Williams	6/29 9am
2	E.F. Williams/ETC	E.F. Williams	Paul H. R. [Signature]	6/29 2pm

CALIBRATION DATA

DRY GAS METER CALIBRATION

Meter I.D. RAC 591249

Date 6-22-85

Calibration Method DGM/DGM Bell Pneu

By DGR

Calibration Meter I.D. 651725

Barometric Pressure 30.00

Previous use: _____

Vac			Calibrating Meter			Field Meter					Y	
In.	In.	Time	VI	VF	Temp	VI	VF	Temp °F				
flg	flg	min	cf	cf	°f	cf	cf	In		out		
5	2.00	19.5	102.487	116.231	72	262.662	277.372	96	115	96	93	9787
5	2.00	16.0	116.231	127.800	72	272.372	289.724	115	122	95	96	9828
5	2.00	95.5	127.800	196.549	71	289.724	364.373	119	135	97	109	9924
												9887
												99

$$Y = [(Vcal)(Pbar)(TdgM)] / [(Vdgm)(Pm)(Tcal)]$$

Where:

Y = Meter correction factor

Vcal = Volume of gas through calibrating meter, ft.³

Vdgm = Volume of gas through field dry gas meter, ft.³

Pbar = Barometric pressure, In. Hg

Pm = Meter pressure, (Pbar+UI/13.6); In. Hg

TdgM = Average Dry gas meter temp.; °R

Tcal = Temperature of gas through calibrating meter; °R

DRY GAS METER CALIBRATION

Meter I.D. RAC 591349

Date 2-2-89

Calibration Method DCM / DCM Burette

By DGR

Calibration Meter I.D. 651229

Barometric Pressure 30.08

Previous use: 5 point calibration following overhaul on 2-1-89

Vac In.	Oil In.	Time min.	Calibrating Meter			Field Meter					Y
			VI cf	VF cf	Temp °F	VI cf	VF cf	Temp °F			
Hg	H ₂ O							In	out		
1	4.00	10'0"	491.709	501.830	70	491.896	492.318	72:46	72:23	.9762	2.095
1	3.00	10'55"	501.830	511.559	71	492.118	492.346	96:10	72:78	.9944	2.119
1	2.00	13'21"	511.559	521.337	71	492.346	502.558	105:11	76:83	.9919	2.075
1	1.50	15'2"	521.337	530.971	71	502.558	512.560	107:11	81:86	.6005	2.084
1	1.00	16'12"	530.971	540.472	71	512.560	522.564	111:11	87:42	.6003	1.619
										.55	1.992

$$Y = [(Vcal)(Pbar)(Tdg)] / [(Vdgm)(Pm)(Tcal)]$$

Where:

Y = Meter correction factor

Vcal = Volume of gas through calibrating meter; ft.³

Vdgm = Volume of gas through Field dry gas meter; ft.³

Pbar = Barometric pressure; In; Hg

Pm = Meter pressure; (Pbar+Oil/13.6); In; Hg

Tdg = Average Dry gas meter temp., °R

Tcal = Temperature of gas through calibrating meter; °R

THERMOMETER/THERMOCOUPLE CALIBRATION

Date: 6-19-89By: JGRReference Thermometer ASTM Hz/gas 20° - 760° F

Last Service _____

Field Thermometer	Temp. Source	Reference Temperature	Field Therm: Temperature	% error, absolute
3' T'couple Omega 650	RSB stack	121	124	<1
Meter In Omega 650	Ambient	85	85	-
Meter Out Omega 650	Ambient	85	85	-
Impinger out Bimetal-dial	Ambient	85	87	<1
Sample Box Bimetal-dial	Box No. 1	238	230	2

PITOT TUBE GEOMETRY CALIBRATION

Pitot tube/probe identification: 3' Q

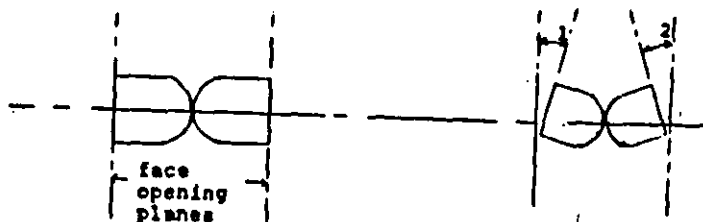
Date Checked: 6-22-85 By: PCN

1. Pitot tubes having the following geometric characteristics are assigned a pitot tube coefficient of 0.84.

1. Face openings perpendicular to transverse axis: (α_1 and $\alpha_2 < 10^\circ$)

$\alpha_1 =$ 0

$\alpha_2 =$ 0



2. Face openings parallel to longitudinal axis: (β_1 and $\beta_2 \leq 5^\circ$; $P = 1.05 D_t$ to $1.50 D_t$; $P_A = P_B$)

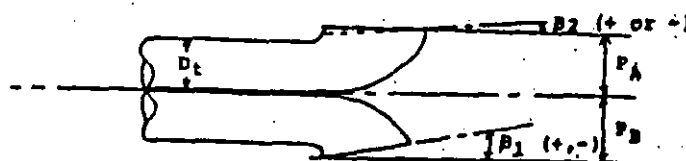
$D_t =$.375

$\beta_1 =$ 0

$P_A =$.450

$\beta_2 =$ 0

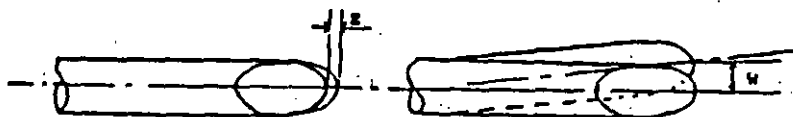
$P_B =$.450



3. Both legs equal length and centerline coincident ($z < .125$ inch; $w < .031$ inch)

$z =$ 0

$w =$ 0



PITOT/PROBE CLEARANCE CHECK:

Nozzle ID: .195

Nozzle dia: .195

Date: 6-22-89

11. Pitot/probe/nozzle assemblies have the same C_p as the Isolated Pitot tube when the following conditions exist.

1. $D_t > .188$ & $< .375$ inch

$D_t =$.375 "

2. $X_1 \geq .75$ inch

$X_1 =$.90 "

3. $X_2 \geq 0$ inch

$X_2 =$.8 "

4. $Y \geq 3.0$ inch

$Y =$ 6.2 "

5. $Z \geq 2.0$ inch

$Z =$ 2.35 "

