

Note: This is a reference cited in *AP 42, Compilation of Air Pollutant Emission Factors, Volume I Stationary Point and Area Sources*. AP42 is located on the EPA web site at www.epa.gov/ttn/chief/ap42/

The file name refers to the reference number, the AP42 chapter and section. The file name "ref02_c01s02.pdf" would mean the reference is from AP42 chapter 1 section 2. The reference may be from a previous version of the section and no longer cited. The primary source should always be checked.

Background Report Reference

AP-42 Section Number: 12.20

Background Chapter: 4

Reference Number: 53

Title: Source Test Report No. 86-0256 of
Plato Products, Inc., 2120 East Allen
Avenue, Glendora, CA

Truesdail Laboratories

July 1987

South Coast Air Quality Management District

Source Test Report 87-0256

Plate Products Inc.
2120 East Allen Avenue
Glendora, California

29 July 1987

UNACCEPTABLE

The inlet data on this report are acceptable but the outlet testing looks sloppy. There are no meter temperatures on the outlet field data sheet except for three spaces towards the bottom of the sheet which give the temperature at 106-107 degrees F. This does not agree with the temperature given on the calculation sheet in the front of the report. The static pressure for the stack is not given on the outlet sheet. There are no individual stack temperatures recorded on the field data sheets, and the two temperatures given on the sheet do not average to the same temperature given on the calculation sheet.

On this particular test, the time of the test was 480 minutes. The inlet location had 24 points while the outlet had only 12. If the points are greater than 5 minutes in duration, the points should be read at least every five minutes.

The CO2 in this test looks suspiciously high. Ambient air is the source for this process and no combustion takes place. There is no mention of how this value was obtained but it appears that a decimal may have been misplaced or that something was wrong with the ORSAT if one was used.

Although the report says that this was a test of a scrubber, the drawing in the report of the sampling locations shows a filter box after the scrubber. The test is a scrubber/filter box combination and not simply just a scrubber. The filter box probably accounts for the lower flow at the outlet when compared with the inlet.

3/1/89
MEMORANDUM

SUBJECT: Acceptability of Test Reports for use as a Data Base for Chromium NESHAP

FROM: Frank R. Clay

TO: Dallas Safriet
Pollutant Characterization Section (MD-15)

I have reviewed the following four test reports and have found them unacceptable for use in the Data Base for the Chromium NESHAP. The reasons that the reports are unacceptable are also given.

The reports have been returned to Andy Smith.

cc: Andy Smith

SAMPLING SUMMARY SHEET

PLANT Plato Products

LOCATION Los Angeles, Calif.

SAMPLED SOURCE Scrubber Inlet and Outlet

Run	Date	N _p	Y _m	ΔH	P Bar.	V _m	T _m	V _m Std.	%	P _{st}	P _s	T _s	VP	V _w	V _w gas	%M	M _d
1	Inlet 29 Jul 87	224	1.000	0.28	29.08	216.979	60.0	214.368		-1.0	29.01	78.0		70	3.29	1.51	985
1	Outlet 29 Jul 87	12	.9940	.58	29.08	291.710	106	263.287		0.0	29.08	68.0		96	4.52	1.49	983
							60	286.574		0.0		70				1.55	984

Run	(24) CO ₂	(25) O ₂	(26) N ₂	(27) CO	(28) —	(29) MW _d	(30) MW	(31) $C_p \sqrt{A P_s (T_s + 460)}$	(32) $\frac{(31)}{(32)}$	(33) T _t	(34) D _n	(35) V _s	(36) D _s	(37) Area	(38) ACFM	(39) DSCFM	%I
1	Inlet 1.74	21	77.3			29.12	28.95	.846	15.0195	480	.197	37.5	16.0	1.40	3146	2943	100.2
1	Outlet 1.76	21	77.2			29.12	28.93	.846	12.0743	480	.250	30.1	16.0	1.40	2522	2410	93.3
						29.12	28.95		12.1025			30.2			2527	2409	101.6

$V_m \text{ Std.} = Y_m \frac{17.64 \times V_m (P \text{ Bar.} + \frac{\Delta H}{13.6})}{(T_m + 460)}$
 $ZM = \frac{100 \times V_{w \text{ gas}}}{V_m \text{ Std.} + V_{w \text{ gas}}}$
 $M_d = \frac{100 - ZM}{100}$
 $V_{w \text{ gas}} = 0.0471 V_m$
 $MW_d = XCO_2 \times .44 + (XO_2 \times .32) + (XCO + XN_2) \times .28 + (Xother \times Mol. \text{ wt.}) \times \frac{100}{100}$
 $MW = MW_d \times M_d + 18(1 - M_d)$
 $V_s = 85.49 \times C_p \sqrt{P_s (T_s + 460)} \left[\frac{1}{P_s \times MW} \right]^{1/2}$
 $ZI = \frac{0.09450 \times (T_s + 460) \times V_m \text{ Std.}}{V_s \times T_s \times P_s \times M_d \times A_n}$
 $V_p = \text{Vapor Pressure of H}_2\text{O at Stack Temperature}$
 $V_{w \text{ gas}} = \text{Total H}_2\text{O Collected in Impingers and Silica Gel}$
 $V_{w \text{ gas}} = \text{Volume of water vapor collected at STP, SCF}^b$
 $ZM = \text{Per Cent Moisture by volume}$
 $M_d = \text{Mole Fraction of Dry Gas}$
 $XCO_2 = \text{Volume \% Dry}$
 $XO_2 = \text{Volume \% Dry}$
 $XN_2 = \text{Volume \% Dry}$
 $XCO = \text{Volume \% Dry}$
 $MW_d = \text{Molecular Weight of Stack Gas Dry Basis}$
 $MW = \text{Molecular Weight of Stack Gas, Wet Basis}$
 $C_p = \text{Pitot Tube Coefficient}$
 $V_p = \text{Vapor Pressure of H}_2\text{O at Stack Temperature}$
 $V_{w \text{ gas}} = \text{Total H}_2\text{O Collected in Impingers and Silica Gel}$
 $V_{w \text{ gas}} = \text{Volume of water vapor collected at STP, SCF}^b$
 $ZM = \text{Per Cent Moisture by volume}$
 $M_d = \text{Mole Fraction of Dry Gas}$
 $XCO_2 = \text{Volume \% Dry}$
 $XO_2 = \text{Volume \% Dry}$
 $XN_2 = \text{Volume \% Dry}$
 $XCO = \text{Volume \% Dry}$
 $MW_d = \text{Molecular Weight of Stack Gas Dry Basis}$
 $MW = \text{Molecular Weight of Stack Gas, Wet Basis}$
 $C_p = \text{Pitot Tube Coefficient}$
 $V_p = \text{Vapor Pressure of H}_2\text{O at Stack Temperature}$
 $V_{w \text{ gas}} = \text{Total H}_2\text{O Collected in Impingers and Silica Gel}$
 $V_{w \text{ gas}} = \text{Volume of water vapor collected at STP, SCF}^b$
 $ZM = \text{Per Cent Moisture by volume}$
 $M_d = \text{Mole Fraction of Dry Gas}$
 $XCO_2 = \text{Volume \% Dry}$
 $XO_2 = \text{Volume \% Dry}$
 $XN_2 = \text{Volume \% Dry}$
 $XCO = \text{Volume \% Dry}$
 $MW_d = \text{Molecular Weight of Stack Gas Dry Basis}$
 $MW = \text{Molecular Weight of Stack Gas, Wet Basis}$
 $C_p = \text{Pitot Tube Coefficient}$
 $V_p = \text{Vapor Pressure of H}_2\text{O at Stack Temperature}$
 $V_{w \text{ gas}} = \text{Total H}_2\text{O Collected in Impingers and Silica Gel}$
 $V_{w \text{ gas}} = \text{Volume of water vapor collected at STP, SCF}^b$
 $ZM = \text{Per Cent Moisture by volume}$
 $M_d = \text{Mole Fraction of Dry Gas}$
 $XCO_2 = \text{Volume \% Dry}$
 $XO_2 = \text{Volume \% Dry}$
 $XN_2 = \text{Volume \% Dry}$
 $XCO = \text{Volume \% Dry}$
 $MW_d = \text{Molecular Weight of Stack Gas Dry Basis}$
 $MW = \text{Molecular Weight of Stack Gas, Wet Basis}$
 $C_p = \text{Pitot Tube Coefficient}$

SUMMARY OF EMISSIONS

PLANT _____ LOCATION _____

SAMPLED SOURCE _____

RUN	DATE	①		②	
		V _m Std.		DSCFM	

FRONT HALF MILLIGRAMS					③
PROBE	CYCLONE	FILTER	TOTAL		

5 FRONT + BACK TOTAL					④
BACK HALF					

CONCENTRATIONS

RUN	FRONT HALF			
	Gr/DSCF	Mg/M ³	Lb/Hr	Kg/Hr

RUN	BACK HALF			
	Gr/DSCF	Mg/M ³	Lb/Hr	Kg/Hr

RUN	TOTAL			
	Gr/DSCF	Mg/M ³	Lb/Hr	Kg/Hr

6 7 8 9 10 17 18 19 20 21 22 23

Remarks: _____

PLANT Plato San Bern

LOCATION

SAMPLED SOURCE

Run	Date	N _p	Y _m	ΔH	P Bar.	V _m	T _m	V Std.	%	P _{st}	P _s	T _s	VP	V _w	V _{w gas}	%M	M _d
1	Inlet 29 JUL 87	16	1.000	.75	28.84	360.80	81.0	340.067		-76	28.78	73		63	2.97	0.86	.991
1	Outlet 29 JUL 87	16	1.000	.47	28.84	293.34	86.0	273.757		1.01	28.84	68		78	3.67	1.32	.987

Run	CO ₂	O ₂	N ₂	(25)	(26)	(27)	(28)	29	30	31	(32)	(33)	(34)	35	(36)	(37)	38	39	40
									MW	C _p	$\sqrt{P_s(T_s + 460)}$	T _t	D _n	V _s	D _s	Area	ACFM	DSCFM	%I
1	Inlet 0.7	21.0	78.3					28.86	28.86	.84	12.5929	480	.25	31.3	16	1.40	2629	2483	116.9
1	Outlet 0.7	21.0	78.3					28.81	28.81	.84	9.7381	480	.25	24.3	16	1.40	2033	1933	120.9

$$V_m \text{ Std.} = Y_m \frac{17.64 \times V_m (P \text{ Bar.} + \frac{\Delta H}{13.6})}{(T_m + 460)}$$

$$XH = \frac{100 \times V_m}{V_m \text{ Std.} + V_{w \text{ gas}}}$$

$$M_d = \frac{100 - XH}{100}$$

$$V_{w \text{ gas}} = 0.0471 V_m$$

$$MW_d = XCO_2 \times .44 + (XO_2 \times .32) + (XCO + XN_2) \times .28 + (Xother \times Mol. wt. / 100)$$

$$MW = MW_d \times M_d + 18(1 - M_d)$$

$$V_s = 85.49 \times C_p \sqrt{P_s (T_s + 460)} \left[\frac{1}{P_s \times MW} \right]^{1/2}$$

$$XI = \frac{0.09450 \times (T_s + 460) \times V_m \text{ Std.}}{V_s \times T_s \times P_s \times M_d \times A_n}$$

$$N_p = \text{Total No. of Sampling points}$$

$$X_m = \text{Meter Box Correction Factor}$$

$$\Delta H = \text{Average Orifice Pressure Drop, inches H}_2\text{O}$$

$$P \text{ Bar.} = \text{Barometric Pressure, inches Hg, Absolute}$$

$$V_m = \text{Volume of Dry Gas at Meter Conditions, DCF}$$

$$T_m = \text{Average Meter Temperature, } ^\circ\text{F.}$$

$$V_m \text{ Std.} = \text{Volume of Dry Gas at STP, DSCFM}$$

$$X = \text{Per Cent other gas removed before Dry Gas Meter}$$

$$P_{st} = \text{Static Pressure of Stack Gas, inches H}_2\text{O}$$

$$P_s = \text{Stack Gas Pressure, inches Hg.}$$

$$T_s = \text{Average Stack Temperature, } ^\circ\text{F.}$$

$$VP = \text{Vapor Pressure of H}_2\text{O at Stack Temperature}$$

$$V_{w \text{ gas}} = \text{Total H}_2\text{O Collected in Impinger and Silica Gel}$$

$$V_{w \text{ gas}} = \text{Volume of water vapor collected at STP, SCF}$$

$$XH = \text{Per Cent Moisture by volume}$$

$$M_d = \text{Mole Fraction of Dry Gas}$$

$$XCO_2 = \text{Volume \% Dry}$$

$$XO_2 = \text{Volume \% Dry}$$

$$XN_2 = \text{Volume \% Dry}$$

$$XCO = \text{Volume \% Dry}$$

$$MW_d = \text{Molecular Weight of Stack Gas Dry Basis}$$

$$MW = \text{Molecular Weight of Stack Gas, Wet Basis,}$$

$$C_p = \text{Pitot Tube Coefficient}$$

$$\sqrt{A \cdot P (T + 460)}$$
 is determined by averaging the square root of the product of the velocity head (P) and the absolute stack temperature from each sampling point.

$$T_t = \text{Net time of test in minutes}$$

$$D_n = \text{Sampling Nozzle Diameter, inches}$$

$$A_n = \text{Area of Nozzle opening, ft}^2$$

$$V_s = \text{Stack Gas Velocity at Stack Conditions, Feet per second.}$$

$$D_s = \text{Diameter of Stack, inches}$$

$$\text{Area} = \text{Area of duct in ft}^2$$

$$\text{ACFM} = \text{Actual Cubic Feet per minute}$$

$$\text{DSCFM} = \text{Dry Standard Cubic Feet per minute}$$

$$XI = \text{Per Cent Isokinetic}$$

$$^a \text{Dry Standard Cubic Feet @ } 68^\circ\text{F, } 29.92 \text{ in. Hg.}$$

$$^b \text{Standard Conditions @ } 60^\circ\text{F, } 29.92 \text{ in. Hg.}$$

SUMMARY OF EMISSIONS

PLANT _____ LOCATION _____

SAMPLED SOURCE _____

RUN	DATE	1		2	
		V _m Std.		DSCFM	

FRONT HALF MILLIGRAMS				
PROBE	CYCLONE	FILTER	3	
TOTAL				

4		5	
BACK HALF		FRONT + BACK TOTAL	

CONCENTRATIONS

FRONT HALF				
RUN	Gr/DSCF	Mg/M ³	Lb/Hr	Kg/Hr

BACK HALF				
Gr/DSCF	Mg/M ³	Lb/Hr	Kg/Hr	

TOTAL				
Gr/DSCF	Mg/M ³	Lb/Hr	Kg/Hr	

6 7 8 9 10 17 18 19 20 21 22 23

Remarks: _____

XROM "METH 5"

RUN NUMBER		
METER BOX Y?		RUN
DELTA H?		RUN
BAR PRESS ?	.7500	RUN
METER VOL ?	28.8400	RUN
MTR TEMP F?	360.8000	RUN
STATIC HOH IN ?	81.0000	RUN
STACK TEMP.	-7.0000	RUN
ML. WATER ?	73.0000	RUN
% MOISTURE ?	4.5400	RUN

SAT % = 2.8

IMP. % HOH = 0.0

% HOH=2.8

% CO2?

% OXYGEN?

MWd =28.95
MW WET=28.64

PITOT CP ?

SQRT PSTS ?

TIME MIN ?

NOZZLE DIA ?

STK DIA INCH ?

* VOL MTR STD = 340.067
STK PRES ABS = 28.78
VOL HOH GAS = 0.00
% MOISTURE = 2.84
MOL DRY GAS = 0.972
% NITROGEN = 78.30
MOL WT DRY = 28.95
MOL WT WET = 28.64
VELOCITY FPS = 31.50
STACK AREA = 1.40
STACK ACFM = 2,639.
* STACK DSCFM = 2,443.
% ISOKINETIC = 118.85

END OF FIELD DATA

Inlet

XROM "METH 5"

RUN NUMBER		
METER BOX Y?		RUN
DELTA H?		RUN
BAR PRESS ?	.7500	RUN
METER VOL ?	28.8400	RUN
MTR TEMP F?	360.8000	RUN
STATIC HOH IN ?	81.0000	RUN
STACK TEMP.	-7.0000	CLX
ML. WATER ?	73.0000	RUN
% MOISTURE ?	4.5400	RUN

SAT % = 2.8

IMP. % HOH = 0.0

% HOH=2.8

% CO2?

% OXYGEN?

MWd =28.95
MW WET=28.45

PITOT CP ?

SQRT PSTS ?

TIME MIN ?

NOZZLE DIA ?

STK DIA INCH ?

* VOL MTR STD = 340.067
STK PRES ABS = 28.78
VOL HOH GAS = 0.00
% MOISTURE = 4.54
MOL DRY GAS = 0.955
% NITROGEN = 78.30
MOL WT DRY = 28.95
MOL WT WET = 28.45
VELOCITY FPS = 31.60
STACK AREA = 1.40
STACK ACFM = 2,647.
* STACK DSCFM = 2,408.
% ISOKINETIC = 120.57

END OF FIELD DATA

Inlet

XROM "METH 5"

RUN NUMBER		
METER BOX Y?		RUN
DELTA H?		RUN
BAR PRESS ?	.7500	RUN
METER VOL ?	28.8400	RUN
MTR TEMP F?	360.8000	RUN
STATIC HOH IN ?	81.0000	RUN
STACK TEMP.	-7.0000	RUN
ML. WATER ?	63.0000	RUN

SAT % = 2.8

IMP. % HOH = 0.9

% HOH=0.9

% CO2?

% OXYGEN?

MWd =28.95
MW WET=28.86

PITOT CP ?

SQRT PSTS ?

TIME MIN ?

NOZZLE DIA ?

STK DIA INCH ?

* VOL MTR STD = 340.067
STK PRES ABS = 28.78
VOL HOH GAS = 2.97
% MOISTURE = 0.86
MOL DRY GAS = 0.991
% NITROGEN = 78.30
MOL WT DRY = 28.95
MOL WT WET = 28.86
VELOCITY FPS = 31.38
STACK AREA = 1.40
STACK ACFM = 2,629.
* STACK DSCFM = 2,483.
% ISOKINETIC = 116.92

END OF FIELD DATA

Inlet

XROM "METH 5"

RUN NUMBER	
METER BOX Y?	RUN
DELTA H?	RUN
.4700	RUN
BAR PRESS ?	
28.8400	RUN
METER VOL ?	
293.3400	RUN
MTR TEMP F?	
86.0000	RUN
STATIC HOH IN ?	
.0100	RUN
STACK TEMP.	
68.0000	RUN
ML. WATER ?	
	RUN
% MOISTURE ?	
2.9000	RUN

SAT % = 2.4

IMP. % HOH = 0.0

% HOH=2.4

% CO2?

2.9000 STO 22

.7000 RUN

% OXYGEN?

21.0000 RUN

MWD =28.95

MW WET=28.63

PITOT CP ?

.8400 RUN

SQRT PSTS ?

9.7381 RUN

TIME MIN ?

480.0000 RUN

NOZZLE DIA ?

.2500 RUN

STK DIA INCH ?

16.0000 RUN

* VOL MTR STD = 273.757

STK PRES ABS = 28.84

VOL HOH GAS = 0.00

% MOISTURE = 2.90

MOL DRY GAS = 0.971

% NITROGEN = 78.30

MOL WT DRY = 28.95

MOL WT WET = 28.63

VELOCITY FPS = 24.33

STACK AREA = 1.40

STACK ACFM = 2.039.

* STACK DSCFM = 1.908.

% ISOKINETIC = 122.50

END OF FIELD DATA

XROM "METH 5"

RUN NUMBER	
METER BOX Y?	RUN
DELTA H?	RUN
.4700	RUN
BAR PRESS ?	
28.8400	RUN
METER VOL ?	
293.3400	RUN
MTR TEMP F?	
86.0000	RUN
STATIC HOH IN ?	
.0100	RUN
STACK TEMP.	
68.0000	RUN
ML. WATER ?	
78.0000	RUN

SAT % = 2.4

IMP. % HOH = 1.3

% HOH=1.3

% CO2?

.7000 RUN

% OXYGEN?

21.0000 RUN

MWD =28.95

MW WET=28.81

PITOT CP ?

.8400 RUN

SQRT PSTS ?

9.7381 RUN

TIME MIN ?

480.0000 RUN

NOZZLE DIA ?

.2500 RUN

STK DIA INCH ?

16.0000 RUN

* VOL MTR STD = 273.757

STK PRES ABS = 28.84

VOL HOH GAS = 0.00

% MOISTURE = 2.90

MOL DRY GAS = 0.987

% NITROGEN = 78.30

MOL WT DRY = 28.95

MOL WT WET = 28.81

VELOCITY FPS = 24.26

STACK AREA = 1.40

STACK ACFM = 2.033.

* STACK DSCFM = 1.933.

% ISOKINETIC = 120.91

END OF FIELD DATA

Outlet Real HOH



**South Coast
AIR QUALITY MANAGEMENT DISTRICT**

9150 FLAIR DRIVE, EL MONTE, CA 91731 (818) 572-8200

SOURCE TEST REPORT

87-0256

CONDUCTED AT

**Plato Products Inc.
2120 E. Allen Ave.
Glendora, CA**

RECEIVED

SEP 05 1987

PLATO-CALIF.

**EFFICIENCY OF, AND EMISSIONS FROM A SCRUBBER SERVING A
HARD CHROME PLATING TANK**

TESTED: July 29, 1987

ISSUED: AUG 24 1987

**REPORT BY: Xuan Vu
Air Quality Engineer II**

REVIEWED BY:

Edward J. Ramirez

E. Ramirez, Senior A.Q. Engineer

Steven Marinoff for

R. Schneider, Supervising A.Q. Engineer

**SOURCE TESTING AND MONITORING BRANCH
John Higuchi, Manager**

**SANFORD M. WEISS
DIRECTOR, TECHNICAL SERVICES DIVISION**

F. Clay

2/22/89

Please review.

SCADMP Report #87-0256

Plato Products

(Not the same as before.

Apparently they tested 2x)

For D. Safirey

A. Smith

SOUTH COAST AIR QUALITY MANAGEMENT DISTRICT
9150 Flair Drive, El Monte, California 91731

Test No. 87-0256

-2-

Date: 7/29/87

INTRODUCTION

- (a) Firm Tested: Plato Products Inc.
- (b) Test Location: 2120 E. Allen Ave., Glendora, CA
- (c) Unit Tested: Scrubber Serving Chrome Plating Tank
- (d) Test Requested by: Tran Vo - Engineering
- (e) Reason for Test Request ..: Engineering Information, Rule 40
- (f) Date of Test: July 29, 1987
- (g) Source Test Performed by : E. Genato, E. Ramirez, C. Bhatt,
X. Vu
- (h) Test Arranged Through ...: R. Hartman (818) 967-3821
- (i) Source Test Observed by ..: Tran Vo - Engineering
- (j) Company I.D. No.....: 045443
- (k) Permit No.....:
- (l) Application No.....:

SOUTH COAST AIR QUALITY MANAGEMENT DISTRICT
9150 Flair Drive, El Monte, California 91731

Test No. 87-0256

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Date: 7/29/87

RESULTS

Flow Rates: Scrubber Inlet 68.5 dscmm (2,418 dscfm)
Scrubber Outlet 81.9 dscmm (2,893 dscfm)

CONTAMINANT	EMISSIONS		APPLICABLE RULE
	MEASURED	ALLOWED	
<u>HEXAVALENT CHROME</u>			
Concentration			
-Scrubber Inlet	3.85 g/dscm (1.68×10^{-6} gr/dscf)	---	Infor.
-Scrubber Outlet	1.88 g/dscm (0.82×10^{-6} gr/dscf)	---	Infor.
Mass Rate			
-Scrubber Inlet	18.9 mg/hr (41.7×10^{-6} lb/hr)	---	Infor.
-Scrubber Outlet	7.71 mg/hr (17.0×10^{-6} lb/hr)	---	Infor.
Blank Loading	5.0 micro-grams	---	Infor.
<u>TOTAL CHROME</u>			
Concentration			
-Scrubber Inlet	4.18 g/dscm (1.83×10^{-6} gr/dscf)	---	Infor.
-Scrubber Outlet	2.00 g/dscm (0.88×10^{-6} gr/dscf)	---	Infor.
Mass Rate			
-Scrubber Inlet	20.6 mg/hr (45.4×10^{-6} lb/hr)	---	Infor.
-Scrubber Outlet	8.23 mg/hr (18.1×10^{-6} lb/hr)	---	Infor.
Blank Loading	1.0 micro-grams	---	Infor.
Scrubber Efficiency	59%	---	Infor.
PARTICULATE MATTER			
Concentration	4.0 mg/dscm (0.002 gr/dscf)	308 mg/dscm (0.135 gr/dscf)	404(a)
Mass Rate	0.02 kg/hr (0.04 lb/hr)	---	Infor.

SOUTH COAST AIR QUALITY MANAGEMENT DISTRICT
9150 Flair Drive, El Monte, California 91731

Test No. 87-0256

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Date: 7/29/87

INTRODUCTION

On July 29, 1987, personnel from the South Coast Air Quality Management District conducted a source test on the inlet and outlet of a cross-flow sprayed water scrubber controlling the exhaust from a hard chrome plating tank operated by Plato Products, Inc. The purpose of the test was to measure any potential toxic emissions of chromium from this tank and from the scrubber.

PROCESS DESCRIPTION

This company specializes in manufacturing soldering iron tips at this location. The process starts with solid copper tips, which are degreased after machining and initially plated with iron. The iron tips are then waxed on the tip, etched with hydrochloric acid and subsequently plated with nickel and chrome on the unwax portion.

The plating bath is a mixture of chromic acid and sulfuric acid solutions kept at 130-140 °F and kept covered with polyethylene beads. The plating is accomplished at 6V and 1300 AMP DC (average). The emissions from this tank are controlled by a cross-flow sprayed water scrubber. The measured water overflow rate from the scrubber was 1.92 GPM and the water recirculation rate was approximately 75 GPM. A process schematic is shown in FIGURE 1.

SAMPLING AND ANALYTICAL PROCEDURES

GAS FLOW RATE

The gas velocities and temperatures at the outlet and the inlet to the scrubber serving the chrome plating tank (designated as chrome scrubber) were measured using a Pitot tube, Magnehelic gage, and an Omega potentiometer with a type "K" thermocouple (FIGURE 2). The gas flow rates were determined from the gas velocity, pressure, temperature, density of the gas and the cross-sectional area of the discharge stack and the inlet duct.

CHROME AND PARTICULATE SAMPLING

A traversed particulate sample was collected isokinetically for 60 minutes at the outlet of the scrubber using Method 5.2 as described in FIGURE 2.

SOUTH COAST AIR QUALITY MANAGEMENT DISTRICT
9150 Flair Drive, El Monte, California 91731

Test No. 87-0256

-5-

Date: 7/29/87

Two chrome samples were collected isokinetically and simultaneously for 480 minutes (8 hours) at the inlet and outlet of the scrubber employing the impingement trains set-up as shown in FIGURE 3.

The inlet was traversed sampled over 24 points at 20 minutes per point. The outlet was traversed sampled over 12 points at 40 minutes per point.

A blank chromium sampling train was brought to the test site, leak checked, and analyzed by the District Chemistry Laboratory. The results were reported in the summary page.

A sample of the plating tank solution was obtained and submitted to the District Chemistry Laboratory along with the samples for analysis of particulate matter, hexavalent chrome, and total chrome.

TEST CRITIQUE

Sampling stopped briefly during the testing period due to a power failure and resumed after the process was stabilized.

The isokinetic sampling rates of 100% were achieved for both inlet and outlet chrome tests. An isokinetic sampling rate of 99% was achieved for particulate test.

The particulate matter test results indicate compliance with District Rule 404(a).

SOUTH COAST AIR QUALITY MANAGEMENT DISTRICT

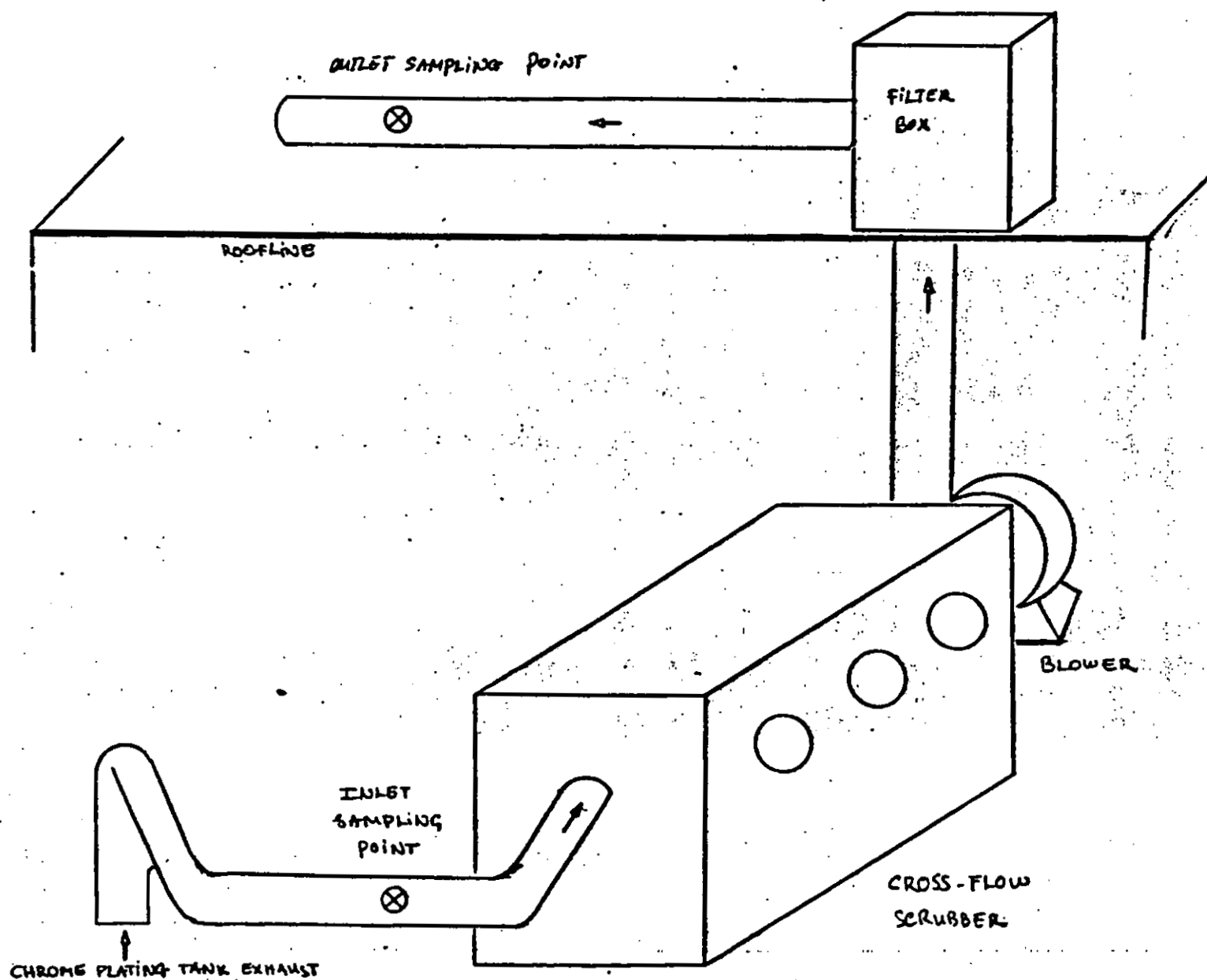
Case No. 87-0256

Date 7-29-87

Figure No. 1

Drawn By X.V.

PROCESS DIAGRAM


Company PLATO PRODUCTS INC.

Process Depicted HARD CHROME PLATING CONTROLLED BY A SCRUBBER

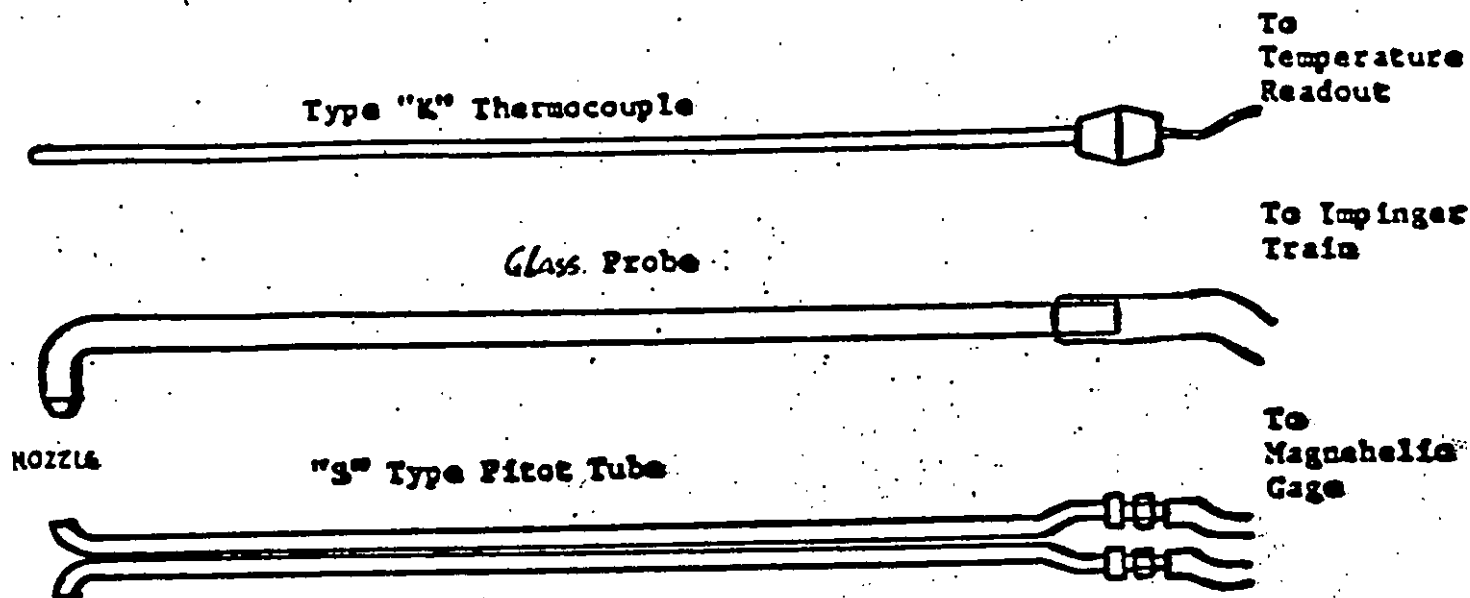
SOUTH EAST AIR QUALITY MANAGEMENT DISTRICT
9150 Flair Drive, El Monte, California 91734

No. 87-0256

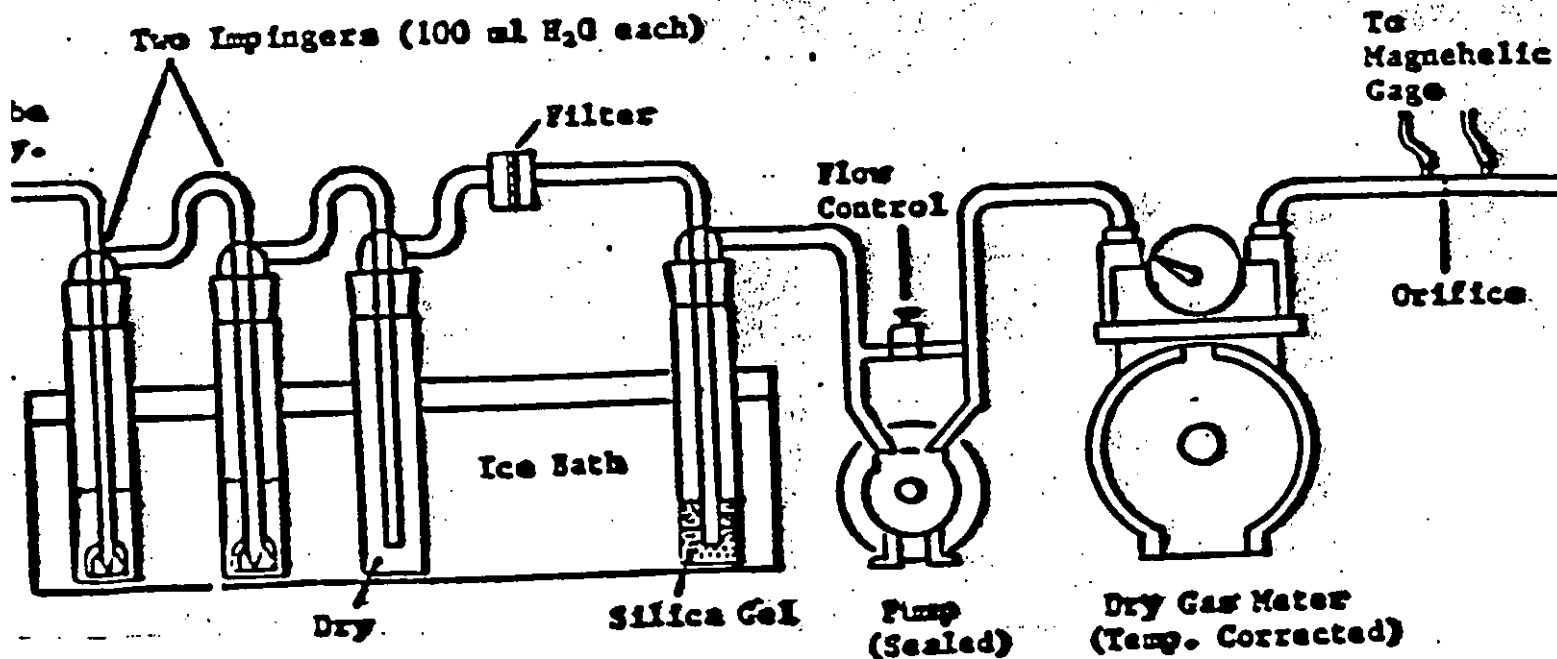
Page No. 7

Date 7-29-87

re No. 2



Probe Set-up



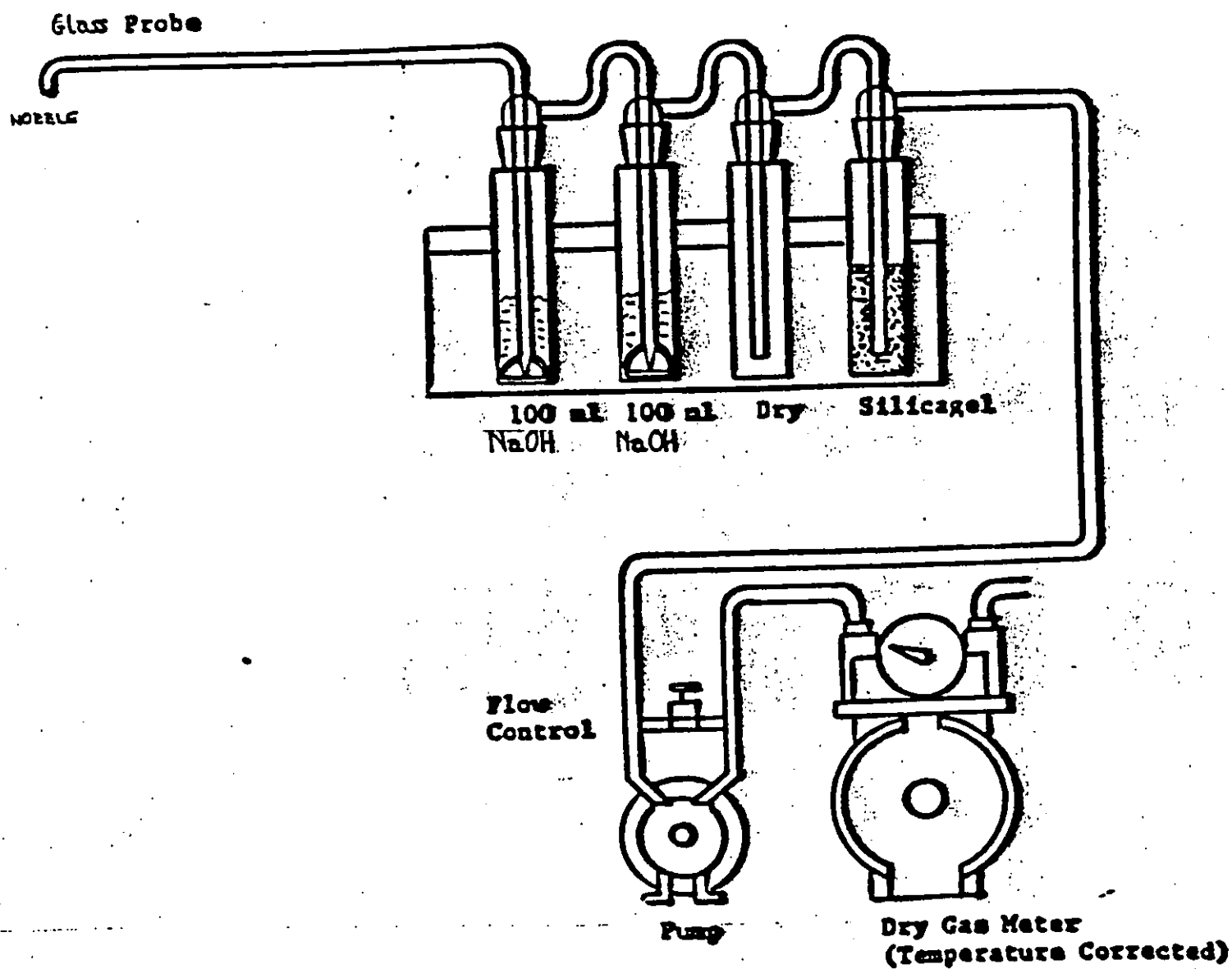
IMPINGER TRAIN SET-UP
(Wet Impingement Method)

No. 87-0256

Page No. 8

Date 7-29-57

e No. 3



CHROME IMPINGER TRAIN SETUP

9.

SOUTH COAST AIR QUALITY MANAGEMENT DISTRICT
TECHNICAL SERVICES DIVISION
SOURCE TESTING AND MONITORING BRANCH
CALCULATION SHEET

Pages	Page
Test No.	Date
87-0256	7/29/87
Processed By	Checked By
Xuan Vu	ER
Sample	CHROMIUM
Train	Scrubber Inlet

SUMMARY

1. Average Traverse Velocity (Pre-Test).....	--	fps
2. Average Reference Point Velocity (pre-test).....	--	fps
3. Average Traverse Velocity (during test).....	43.56	fps
4. Ave. Stack Temp..... 78	°F	K. Water Vapor Condensed... 70 ml
5. Stack Area..... 1.40	ft²	L. Gas Volume Metered..... 216.979dscf
6. Barometric Pressure. 29.08	"HgA	M. Meter Temperature..... 60 °F
7. Stack Pressure..... 29.01	"HgA	N. Average Orifice P..... 0.28 "H₂O
8. Pitot Corr. Factor.. 0.846		O. Meter Calib. Factor..... 1.0004
9. Sampling Time..... 480	min.	P. % CO₂..... 1.74
10. Nozzle Area..... 0.0002117	ft²	Q. % O₂..... 21.0
11. Magnehelic Calibration Factor		1.000
12. Correct Gas Volume Metered	$\frac{L \times (F + N/13.6) \times 520 \times O}{29.92 \times (M + 460)}$	
		211.1 dscf

PERCENT MOISTURE - GAS DENSITY

13. Percent Water In Gas Sample $[4.64 \times K / (0.0464 \times K) + R]$	1.52	%
14. Average Wet Molecular Weights	$0.189 + (1 - S/100)(0.44P + 0.32Q + 0.28(100 - P - Q))$	
	28.95	

FLOW RATE

15. Gas Density Correction Factor $(28.95/T)^{1/2}$	1.000	
16. Flue Correction Factor (A/B).....	1.000	
17. Velocity Pressure Correction Factor $(29.92/Q)^{1/2}$	1.016	
18. Corrected Velocity $(C \times H \times U \times V \times W) (Q')^{1/2}$	37.42	fps
19. Flow Rate $(X \times E \times 60)$	3135	cfm
20. Flow Rate $(Y \times G/29.92 \times 520/(460+D))$	2938	scfm
21A. Flow Rate $[Z \times (1-S/100)]$	2893	dscfm

SAMPLE CONCENTRATION - EMISSION RATE

22B. Total Chromium	25×10^{-3}	mg
23C. Hexavalent Chromium	23×10^{-3}	mg
24D. Total Cr Concentration $(0.01543 \times BB/R)$	1.03×10^{-4}	gr/dscf
25E. Total Cr Emission Rate $(0.00857 \times DD \times AA)$	45.4×10^{-4}	lb/hr
26F. Cr ⁺⁺ Concentration $(0.01543 \times CC/R)$	1.68×10^{-4}	gr/dscf
27G. Cr ⁺⁺ Emission Rate $(0.00857 \times FF \times AA)$	41.7×10^{-4}	lb/hr
28H. Isokinetic Sampling Rate $(E \times R \times V \times 100/I \times J \times AA)$...	100	%

* Corrected for blank loading.

SOUTH COAST AIR QUALITY MANAGEMENT DISTRICT
TECHNICAL SERVICES DIVISION
SOURCE TESTING AND MONITORING BRANCH
CALCULATION SHEET

Pages	Page
Test No.	Date
87-0256	7/29/87
Processed By	Checked By
Xuan Vu	EA
Sample	CHROMIUM
Train	Scrubber Outlet

SUMMARY

Average Traverse Velocity (Pre-Test).....	--	fps
Average Reference Point Velocity (pre-test).....	--	fps
Average Traverse Velocity (during test).....	35.45	fps
Ave. Stack Temp..... 70	°F	
Stack Area..... 1.40	ft²	
Barometric Pressure. 29.08	"HgA	
Stack Pressure..... 29.08	"HgA	
Pitot Corr. Factor.. 0.846		
Sampling Time..... 480	min.	
Nozzle Area..... 0.0003409	ft²	
Magnehelic Calibration Factor		
Correct Gas Volume Metered	$\frac{L \times (F + N/13.6) \times 520 \times Q}{29.92 \times (M + 460)}$	
		282.2 dscf
K. Water Vapor Condensed...	96	ml
L. Gas Volume Metered.....	291.71	dscf
M. Meter Temperature.....	60	°F
N. Average Orifice P.....	0.58	"H₂O
O. Meter Calib. Factor.....	0.994	
P. % CO₂.....	1.76	
Q. % O₂.....	21.0	
	1.000	

PERCENT MOISTURE - GAS DENSITY

Percent Water In Gas Sample $[4.64 \times K / (0.0464 \times K) + R]$	1.55	%
Average Wet Molecular Weight:		
$0.18S + (1 - S/100)(0.44P + 0.32Q + 0.28(100 - P - Q))$	28.95	

LOW RATE

Gas Density Correction Factor $(28.95/T)^{1/2}$	1.000	
Flue Correction Factor (A/B).....	1.000	
Velocity Pressure Correction Factor $(29.92/G)^{1/2}$	1.014	
Corrected Velocity $(C \times H \times U \times V \times W) / (Q')^{1/2}$	30.75	fps
Flow Rate $(X \times E \times 60)$	2576	cfm
Flow Rate $(Y \times G / 29.92 \times 520 / (460 + D))$	2456	scfm
A. Flow Rate $[Z \times (1 - S/100)]$	2418	dscfm

AMPLE CONCENTRATION - EMISSION RATE

B. Total Chromium	16×10^{-3}	mg
C. Hexavalent Chromium	15×10^{-3}	mg
D. Total Cr Concentration $(0.01543 \times BB/R)$	0.88×10^{-4}	gr/dscf
E. Total Cr Emission Rate $(0.00857 \times DD \times AA)$	18.1×10^{-4}	lb/hr
F. Cr ⁺⁺ Concentration $(0.01543 \times CC/R)$	0.82×10^{-4}	gr/dscf
G. Cr ⁺⁺ Emission Rate $(0.00857 \times FF \times AA)$	17.0×10^{-4}	lb/hr
H. Isokinetic Sampling Rate $(E \times R \times V \times 100 / I \times J \times AA)$...	100	%

Corrected for blank loading.

SOUTH COAST AIR QUALITY MANAGEMENT DISTRICT

TECHNICAL SERVICES DIVISION

SOURCE TESTING AND MONITORING BRANCH

CALCULATION SHEET

Pages	Page
Test No.	Date
87-0256	7/29/87
Processed By	Checked By
Xuan Vu	EL
Sample	PARTICULATE
Train	Scrubber Outlet

SUMMARY

Average Traverse Velocity (Pre-Test).....	--	fps
Average Reference Point Velocity (pre-test).....	--	fps
Average Traverse Velocity (during test).....	35.45	fps
Avg. Stack Temp..... 65	°F	
Stack Area..... 1.40	ft ²	
Barometric Pressure. 29.08	"HgA	
Stack Pressure..... 29.08	"HgA	
Pitot Corr. Factor.. 0.855		
Sampling Time..... 60	min.	
Nozzle Area..... 0.0003409ft ²		
Magnehelic Calibration Factor	1.000	
Correct Gas Volume Metered	$L \times (F + N/13.6) \times 520 \times D$	
	$29.92 \times [M + 460]$	34.96 dscf
K. Water Vapor Condensed...	15	ml
L. Gas Volume Metered.....	36.334	dscf
M. Meter Temperature.....	60	°F
N. Average Orifice P.....	0.60	"H ₂ O
O. Meter Calib. Factor.....	0.9884	
P. % CO ₂	2.14	
Q. % O ₂	21	

PERCENT MOISTURE - GAS DENSITY

Percent Water In Gas Sample $[4.64 \times K / (0.0464 \times K) + R]$	2.08	%
Average Wet Molecular Weight:		
$0.18S + (1 - S/100)(0.44P + 0.32Q + 0.28(100 - P - Q))$	28.95	

LOW RATE

Gas Density Correction Factor $(28.95/T)^{1/2}$	1.000	
Flue Correction Factor (A/B).....	1.000	
Velocity Pressure Correction Factor $(29.92/G)^{1/2}$	1.014	
Corrected Velocity $(C \times H \times U \times V \times W) (Q')^{1/2}$	30.75	fps
Flow Rate $(X \times E \times 60)$	2576	cfm
Flow Rate $(Y \times G/29.92 \times 520/(460+D))$	2456	scfm
A. Flow Rate $[Z \times (1-S/100)]$ (From Particulate Calc.)	2400	dscfm

SAMPLE CONCENTRATION - EMISSION RATE

B. Total Particulate	4	mg
C. Solid Particulate	4	mg
D. Sample Concentration $(0.01543 \times BB/R)$	0.002	gr/dscf
E. Sample Emission Rate $(0.00857 \times DD \times AA)$		lb/hr
F. Solid Emission Rate $(1.322 E-4 \times CC \times AA/R)$	0.04	Lb/hr
G. Isokinetic Sampling Rate $(E \times R \times V \times 100/I \times J \times AA)$	99	

SOUTH COAST AIR QUALITY MANAGEMENT DISTRICT

12:

Test No. 87-0256

Date: 7/29/87

Sampling Location: Plato skidder inlet

Sample Train cr

TRAVERSE SOURCE TEST DATA

Pre-Test Leak Check:

Post-Test Leak Check:

Filter cfm @ "Hg vac

Filter cfm @ "Hg vac

Probe 0 cfm @ 18 "Hg vac

Probe 0 cfm @ 12 "Hg vac

(Pitot Tube Leak Check ✓)

(Pitot Tube Leak Check ✓)

Time	Sample Point	Gas Meter Reading (dcf)	Stack		Calculated			Probe Temp. °F	Filter Temp. °F	Meter Temp °F		Vacuum "Hg
			Velocity Head ("H ₂ O)	Temp. °F	Velocity (fps)	Sampling Rate (cfm)	Orifice ΔP ("H ₂ O)			In	Out	
6:35	1	387.090	0.43	78	44.11	0.43	0.29				60	
	2	396.00	0.45	"	45.12	0.44	0.30				"	
	3	406.40	0.49	"	47.09	0.46	0.33				"	
	4	415.75	0.50	"	47.56	0.47	0.33				"	
20 min per point	5	425.40	0.49	"	47.09	0.46	0.33				"	
	6	434.60	0.44	"	44.62	0.44	0.29				"	
	7	443.76	0.37	"	40.92	0.40	0.25				"	
	8	452.75	0.37	"	40.92	0.40	0.25				"	
	9	461.47	0.37	"	40.92	0.40	0.25				"	
	10	469.95	0.37	"	40.92	0.40	0.25				"	
	11	478.28	0.36	"	40.36	0.40	0.24				"	
	12	486.59	0.36	"	40.36	0.40	0.24				"	
10:40	13	494.87										
	14	503.95	0.41	"	43.07	0.42	0.27				"	
	15	512.90	0.41	"	43.07	0.42	0.27				"	
	16	521.84	0.43	"	44.11	0.43	0.29				"	
	17	530.85	0.45	"	45.12	0.44	0.30				"	
	18	539.61	0.44	"	44.62	0.44	0.29				"	
	19	548.42	0.39	"	42.01	0.41	0.26	551.485			"	
	20	557.46	0.37	"	40.92	0.40	0.25	551.485			"	
	21	566.42	0.39	"	42.01	0.41	0.26	551.485			"	
	22	575.26	0.43	"	44.11	0.43	0.29	551.485			"	
	23	585.26	0.46	"	45.62	0.45	0.31	551.485			"	
	24	594.65	0.46	"	45.62	0.45	0.31	551.485			"	
10:52	24	604.06A	0.45	"	45.12	0.44	0.30				"	

(Net Vol. Uncorr.)

Avg.

Nozzle # N/R

Nozzle Diameter mm (0.197 ")

Barometric Pressure 29.02 "HgA

Static Pressure in Stack

Recorded By X Vu

Pitot Factor 0.846

"HgA (+1.0 "H₂O)

Calibration Data

Magnehelic No. 20606 (Cal: 3/11/87)

Pitot Tube No. 20402 (Cal: 1/23/87)

Potentiometer No. 20302 (Cal: 7/8/87)

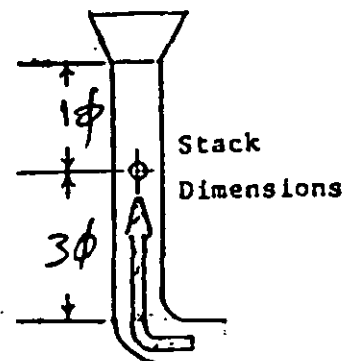
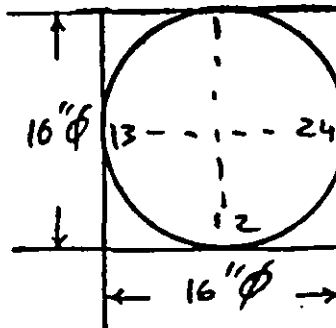
Thermocouple No. 20108 (Cal: 7/8/87)

Gas Meter No. 20702 (Cal: 7-9-87)

Meter Corr. Factor: 1.0004

Purol - 2B

Type Sampling Probe glass



XROM "METH 5"

RUN NUMBER		RUN
METER BOX Y?		RUN
1.0004	RUN	
DELTA H?		RUN
.2800	RUN	
BAR PRESS ?		RUN
29.0000	RUN	
METER VOL ?		RUN
216.9790	RUN	
MTR TEMP F?		RUN
60.0000	RUN	
STATIC HOH IN ?		RUN
-1.0000	RUN	
STACK TEMP.		RUN
70.0000	RUN	
ML. WATER ?		RUN
70.0000	RUN	

SAT % = 3.3

IMP. % HOH = 1.5

% HOH=1.5

% CO2?

.7000	RUN
% OXYGEN?	
21.0000	RUN

MWd =28.95
MW WET=28.79

PITOT CP ?		RUN
.8460	RUN	
SORT PSTS ?		RUN
15.0195	RUN	
TIME MIN ?		RUN
400.0000	RUN	
NOZZLE DIA ?		RUN
.1970	RUN	
STK DIA INCH ?		RUN
16.0000	RUN	

* VOL MTR STD = 214.368
STK PRES ABS = 29.01
VOL HOH GAS = 3.29
% MOISTURE = 1.51
MOL DRY GAS = 0.985
% NITROGEN = 78.30
MOL WT DRY = 28.95
MOL WT WET = 28.79
VELOCITY FPS = 37.59
STACK AREA = 1.40
STACK ACFM = 3.149.
* STACK DSCFM = 2.451.
% ISOKINETIC = 22.89

END OF FIELD DATA

XROM "METH 5"

RUN NUMBER		RUN
METER BOX Y?		RUN
1.0004	RUN	
DELTA H?		RUN
.2800	RUN	
BAR PRESS ?		RUN
29.0000	RUN	
METER VOL ?		RUN
216.9790	RUN	
MTR TEMP F?		RUN
60.0000	RUN	
STATIC HOH IN ?		RUN
-1.0000	RUN	
STACK TEMP.		RUN
70.0000	RUN	
ML. WATER ?		RUN
70.0000	RUN	

SAT % = 3.3

IMP. % HOH = 1.5

% HOH=1.5

% CO2?

1.7400	RUN
% OXYGEN?	
21.0000	RUN

MWd =29.12
MW WET=28.95

PITOT CP ?		RUN
.8460	RUN	
SORT PSTS ?		RUN
15.0195	RUN	
TIME MIN ?		RUN
400.0000	RUN	
NOZZLE DIA ?		RUN
.1970	RUN	
STK DIA INCH ?		RUN
16.0000	RUN	

* VOL MTR STD = 214.368
STK PRES ABS = 29.01
VOL HOH GAS = 3.29
% MOISTURE = 1.51
MOL DRY GAS = 0.985
% NITROGEN = 77.26
MOL WT DRY = 29.12
MOL WT WET = 28.95
VELOCITY FPS = 37.49
STACK AREA = 1.40
STACK ACFM = 3.149.
* STACK DSCFM = 2.943.
% ISOKINETIC = 100.17

END OF FIELD DATA

Date: 7-29-87

Sample Train C_k - train

TRAVERSE SOURCE TEST DATA

Pre-Test Leak Check:

Filter .009 cfm @ 10 "Hg vac

Probe _____ cfm @ _____ "Hg vac

(Pitot Tube Leak Check _____)

Post-Test Leak Check:

Filter _____ cfm @ _____ "Hg vac

Probe .006 cfm @ 5 "Hg vac

(Pitot Tube Leak Check _____)

[illegible]

(Net Vol. Uncorr)

Avg.

Nozzle # NIR -

Nozzle Diameter _____ min (0.25")

Barometric Pressure 112.8

Static Pressure in Stack.....

Recorded By Egnato

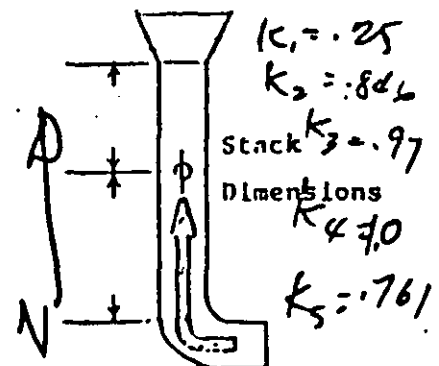
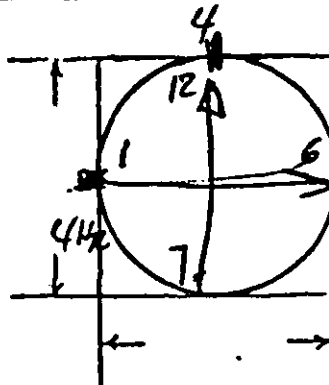
Pitot Factor..... 0.846

"H₂A (+/- "H₂O)

Calibration Data	
Magnehelic No. <u>20627</u>	(Cal: <u>3-11-87</u>)
Pilot Tube No. <u>20402</u>	(Cal: <u>1-23-87</u>)
Potentiometer No. <u>20302</u>	(Cal: <u>7-8-87</u>)
Thermocouple No. <u>20108</u>	(Cal: <u>7-8-87</u>)
Gas Meter No. <u>20703</u>	(Cal: <u>7-9-87</u>)
Meter Corr. Factor: <u>0.9940</u>	

Type Sampling Probe glass

John



SORT PS...

AVE STK TEMP = 70.0000

METER BOX Y? RUN
.9940 RUN
DELTA H? RUN
.5000 RUN
BAR PRESS ? RUN
29.0000 RUN
METER VOL ? RUN
291.7100 RUN
MTR TEMP F? RUN
60.0000 RUN
STATIC HOH IN ? RUN
STACK TEMP. RUN
70.0000 RUN
ML. WATER ? RUN
96.0000 RUN

SAT % = 2.5

IMP. % HOH = 1.6

% HOH=1.6

% CO2?

1.7600 RUN
% OXYGEN? RUN
21.0000 RUN

MWD =29.12
MW WET=28.95

PITOT CP ? RUN
.8460 RUN
SORT PSTS ? RUN
12.1025 RUN
TIME MIN ? RUN
480.0000 RUN
NOZZLE DIA ? RUN
.2500 RUN
STK DIA INCH ? RUN
16.0000 RUN

* VOL MTR STD = 286.574
STK PRES ABS = 29.08
VOL HOH GAS = 4.52
% MOISTURE = 1.55
MOL DRY GAS = 0.984
% NITROGEN = 77.24
MOL WT DRY = 29.12
MOL WT WET = 28.95
VELOCITY FPS = 30.17
STACK AREA = 1.40
STACK ACFM = 2.527.
* STACK DSCFM = 2.409.
% ISOKINETIC = 101.57

END OF FIELD DATA

XROM METH 5"

RUN NUMBER RUN
METER BOX Y? RUN
.9940 RUN
DELTA H? RUN
.5000 RUN
BAR PRESS ? RUN
29.0000 RUN
METER VOL ? RUN
291.7100 RUN
MTR TEMP F? RUN
106.0000 RUN
STATIC HOH IN ? RUN
STACK TEMP. RUN
68.0000 RUN
ML. WATER ? RUN
96.0000 RUN

SAT % = 2.4

IMP. % HOH = 1.7

% HOH=1.7

% CO2?

1.7600 RUN
% OXYGEN? RUN
21.0000 RUN

MWD =29.12
MW WET=28.93

PITOT CP ? RUN
.8460 RUN
SORT PSTS ? RUN
12.0743 RUN
TIME MIN ? RUN
480.0000 RUN
NOZZLE DIA ? RUN
.2500 RUN
STK DIA INCH ? RUN
16.0000 RUN

* VOL MTR STD = 263.283
STK PRES ABS = 29.08
VOL HOH GAS = 4.52
% MOISTURE = 1.69
MOL DRY GAS = 0.983
% NITROGEN = 77.24
MOL WT DRY = 29.12
MOL WT WET = 28.93
VELOCITY FPS = 30.11
STACK AREA = 1.40
STACK ACFM = 2.522.
* STACK DSCFM = 2.410.
% ISOKINETIC = 93.28

DA

DELTA P 8.
STACK TEMP? .36 RUN
FPS = 35. 78. RUN

DELTA P 9.
STACK TEMP? .36 RUN
FPS = 35. 78. RUN

DELTA P 10.
STACK TEMP? .36 RUN
FPS = 35. 78. RUN

DELTA P 11.
STACK TEMP? .36 RUN
FPS = 35. 78. RUN

DELTA P 12.
STACK TEMP? .36 RUN
FPS = 35. 78. RUN

DELTA P 13.
FPS = 38.

DELTA P 14.
FPS = 37.

DELTA P 15.
FPS = 38.

DELTA P 16.
FPS = 39.

DELTA P 17.
FPS = 39.

DELTA P 18.
FPS = 37.

DELTA P 19.
FPS = 36.

DELTA P 20.
FPS = 37.

DELTA P 21.
FPS = 38.

DELTA P 22.
FPS = 39.

DELTA P 23.
FPS = 39.

DELTA P 24.
FPS = 39.

AVE FPS = 38.
AVE FPM = 2,251.
AVE DELTA P = 0.42
STK PRS. ABS = 29.07
AVE STK TEMP = 78.
STACK ACFM = 3,143.
DSCFM = 2,937.

XROM "METH 2"
SITE ?
STACK DIA INCH? RUN
16.0000 RUN
NO TRAY PTS. ?
24.0000 RUN
BAR PRESS ?
29.1400 RUN
STATIC IN HOH ?
-1.0000 RUN
% MOISTURE ?
2.0000 RUN
PITOT CP ?
.8460 RUN
% CO2 ?
1.7400 RUN
% OXYGEN ?
21.0000 RUN
% CO ?
RUN
MOL WT OTHER ?
RUN

MWD = 29.12
MW WET = 28.90

DELTA P 1.
STACK TEMP? .44 RUN
FPS = 38. 78. RUN

DELTA P 2.
STACK TEMP? .45 RUN
FPS = 39. 78. RUN

DELTA P 3.
STACK TEMP? .47 RUN
FPS = 40. 78. RUN

DELTA P 4.
STACK TEMP? .5 RUN
FPS = 41. 78. RUN

DELTA P 5.
STACK TEMP? .5 RUN
FPS = 41. 78. RUN

DELTA P 6.
STACK TEMP? .44 RUN
FPS = 38. 78. RUN

DELTA P 7.
STACK TEMP? .37 RUN
FPS = 35. 78. RUN

SOUTH COAST AIR QUALITY MANAGEMENT DISTRICT

st No. 187-0256Date 7-24-87Sampling Location PLATO SCRUBBER INLET

GAS VELOCITY DATA

Pre-Test Velocity Leak Check ☒Post-Test Velocity Leak Check ☒

Line	Trav. Point	Vel. Head ("H ₂ O)	Temp. (°F)	Calc. Vel. (fps)	Vel. Head ("H ₂ O)	Temp. (°F)	Calc. Vel. (fps)	Vel. Head ("H ₂ O)	Temp. (°F)	Calc. Vel. (fps)
	1	0.44	78		0.44	78		0.42	78	
	2	0.45			0.45			0.45		
	3	0.47			0.49			0.49		
	4	0.50			0.50			0.51		
	5	0.50			0.49			0.48		
	6	0.44			0.44			0.45		
	7	0.37			0.36			0.38		
	8	0.36			0.38			0.38		
	9	0.36			0.37			0.37		
	10	0.36			0.37			0.38		
	11	0.36			0.36			0.36		
	12	0.36	✓		0.35	✓		0.38	✓	
	13	0.42	78		0.40	78		0.40	78	
	14	0.41			0.41			0.41		
	15	0.44			0.42			0.43		
	16	0.46			0.44			0.45		
	17	0.45			0.42			0.44		
	18	0.40			0.36			0.41		
	19	0.38			0.37			0.37		
	20	0.40			0.39			0.39		
	21	0.42			0.44			0.42		
	22	0.46			0.46			0.45		
	23	0.45			0.46			0.46		
	24	0.45	✓		0.46	✓		0.45	✓	

Static Pressure in Stack

"HgA (+10)

1.0 "H₂O)

(Average)

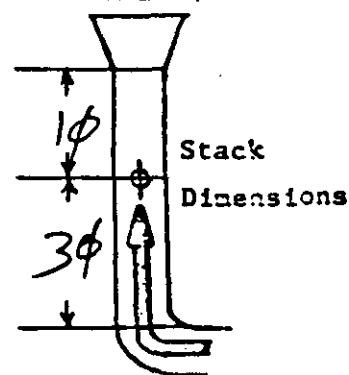
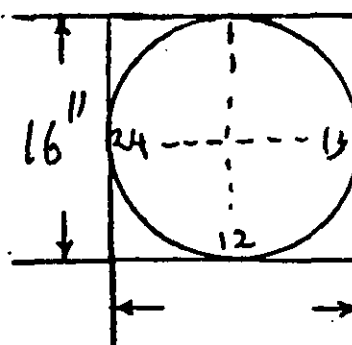
Barometric Pressure..... 29.14 "HgA

Pitot Factor..... 0.846

Recorded By X. Vn

Calibration Data

Magnelic No. 20606 (Cal: 3/11/87)
 Pitot Tube No. 90402 (Cal: 1/23/87)
 Anemometer No. 20702 (Cal: 7/8/87)
 Thermocouple No. 20108 (Cal: 7/8/87)



Date: 7-29-87

Sample Train *PM*

Post-Test Leak Check:

Filter _____ cfm @ _____ "Hg vac

Probe 008 cfm @ 5 'Hg vac

(Pitot Tube Leak Check)

(Net Vol. Uncorr)

Avg.

Nozzle #

Recorded By C. S. Bhatt

Pitot Factor..... 0.855

"H₂A (+/-) _____ "H₂O)

Stack K4 = 1

Dimensions

$K_1 = .25$
 $K_2 = .85$
 $K_3 = .97$
 $K_5 = .71$

Type Sampling Probe Glass

SOUTH COAST AIR QUALITY MANAGEMENT DISTRICT

Test No. 87-0256Date 7/24/87Sampling Location PLATO SCRUBBER OUTLET

GAS VELOCITY DATA

Pre-Test Velocity Leak Check

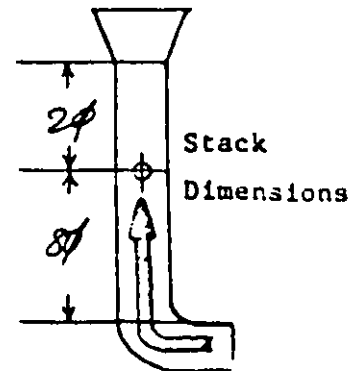
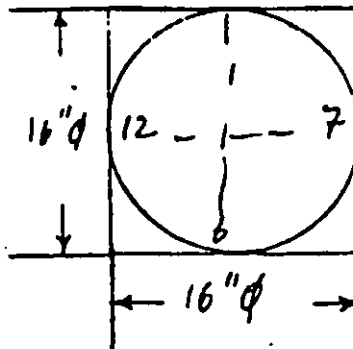
Post-Test Velocity Leak Check

Time	Trav. Point	Vel. Head ("H ₂ O)	Temp. (°F)	Calc. Vel. (fps)	Vel. Head ("H ₂ O)	Temp. (°F)	Calc. Vel. (fps)	Vel. Head ("H ₂ O)	Temp. (°F)	Calc. Vel. (fps)
	1	0.19	70		0.18	70		0.19	70	Ry
	2	0.21	↓		0.22	↓		0.21	↓	.5
	3	0.22	↓		0.22	↓		0.23	↓	.28
	4	0.22	↓		0.22	↓		0.22	↓	.3
	5	0.21	↓		0.22	↓		0.21	↓	.3
	6	0.20	↓		0.20	↓		0.20	↓	.25
	7	0.18	70		0.19	70		0.18	70	0.25
	8	0.21	↓		0.21	↓		0.21	↓	0.28
	9	0.22	↓		0.22	↓		0.22	↓	0.32
	10	0.22	↓		0.22	↓		0.22	↓	0.30
	11	0.22	↓		0.21	↓		0.21	↓	0.30
	12	0.20	↓		0.20	↓		0.20	↓	0.26

Static Pressure in Stack "HgA (+/-) 0.15 "H₂O (Average)Barometric Pressure..... 29.44 "HgAPitot Factor..... 0.846Recorded By K Vm

Calibration Data

Magnehelic No. 20606 (Cal: 3/11/87)
 Pitot Tube No. 20402 (Cal: 1/23/87)
 Potentiometer No. 20302 (Cal: 7/8/87)
 Thermocouple No. 20108 (Cal: 7/8/87)



17.
SOUTH COAST AIR QUALITY MANAGEMENT DISTRICT
9150 Flair Drive, El Monte, California 91731

TECHNICAL SERVICES DIVISION
LABORATORY SERVICES BRANCH
REPORT FOR SOURCE TEST

RELEASED
AUG 11 1987
LAB BRANCH

TO: John Higuchi, Manager
Source Testing & Monitoring

LAB REPORT DATE: August 11, 1987

COMPANY: Plato Products
CITY: Glendora

LABORATORY NO. 82107-11

REFERENCE NO. HMP-1-10, BMC-5-6

PROCESS
EQUIPMENT: Chrome Plating

TEST NO. 87-0256

SOURCE TEST DATE: 7-29-87

CONTROL
EQUIPMENT: Scrubber

DATE SAMPLE RECEIVED: 7-29-87

REQUESTED BY: C.S. Bhatt

SAMPLE DESCRIPTION: 2 scrubber solution bottles

ANALYSIS REQUESTED: Cr^{6+} , Total Chromium

ANALYTICAL WORK PERFORMED, METHOD OF ANALYSIS, AND RESULTS

Cr^{6+} by diphenylcarbazide colorimetric method, total chromium by atomic absorption.

	<u>Scrubber A</u>	<u>Scrubber B</u>
Cr^{6+} , $\mu\text{g/mL}$	0.221	0.219
Total chromium, $\mu\text{g/mL}$	0.221	0.217

TSD RECEIVED
AUG 13 1987
S.T. BRANCH

Approved By:

Greg F. Tott
Margil W. Wadley, Ph.D.
Manager of Laboratory Services

SOUTH COAST AIR QUALITY MANAGEMENT DISTRICT
9150 Flair Drive, El Monte, California 91731

TECHNICAL SERVICES DIVISION
LABORATORY SERVICES BRANCH
REPORT FOR SOURCE TEST

18.
RELEASED
AUG 11 1987
LAB BRANCH

TO: John Higuchi, Manager
Source Testing & Monitoring

LAB REPORT DATE: August 11, 1987

COMPANY: Plato Products, Inc.
CITY: Glendora

LABORATORY NO. 82107-10

REFERENCE NO. HMP-1-10, BMC-5-6

PROCESS
EQUIPMENT: Chrome Plating

TEST NO. 87-0256

SOURCE TEST DATE: 7-29-87

CONTROL
EQUIPMENT: Scrubber

DATE SAMPLE RECEIVED: 7-29-87

REQUESTED BY: C.S. Bhatt

SAMPLE DESCRIPTION: 3 wet impingment trains

ANALYSIS REQUESTED: Cr^{+3} , Total Chromium, moisture gain

ANALYTICAL WORK PERFORMED, METHOD OF ANALYSIS, AND RESULTS

Cr^{+3} by diphenylcarbazide colorimetric method, total chromium by atomic absorption.

	Field Blank	Inlet	Outlet
Reclieved impinger volume, mL	200	236	275
Impinger gain, mL	0	36	75
Silica Gain, g	0	34	21
Cr^{+3} , $\mu g/\mu g$ — μg as per	5	28	20
% recovery Joan	100.7	101.3	101.3
Total chromium, $\mu g/\mu g$ μg 8/11/87 3:25 P	1	26	17

Sample results are not corrected for field blank results. Field blank consists of a train prepared, leak checked, recovered and analyzed in parallel with sample trains.

Approved By:

Joan F. Wadley

Margil W. Wadley, Ph.D.
Manager of Laboratory Services

TSD RECEIVED

AUG 11 1987

S.T. BRANCH

Sender

SOUTH COAST AIR QUALITY MANAGEMENT DISTRICT
9150 Flair Drive, El Monte, California 91731

TECHNICAL SERVICES DIVISION
LABORATORY SERVICES BRANCH
REPORT FOR SOURCE TEST

19.
RELEASED
AUG 18 1987

LAP BRANCH

TO: John Higuchi, Manager
Source Testing & Monitoring

LAB REPORT DATE: August 18, 1987

COMPANY: Plato Products, Inc.
CITY: Glendora

LABORATORY NO. 82107-9

REFERENCE NO. TCH-27-12

PROCESS
EQUIPMENT: Chrome Plating

TEST NO. 87-0256

SOURCE TEST DATE: 7-29-87

CONTROL
EQUIPMENT: Scrubber

DATE SAMPLE RECEIVED: 7-29-87

SAMPLE
DESCRIPTION: One Method 5.1 Train(s)

REQUESTED BY: C. S. Bhatt

ANALYSIS REQUESTED: Particulates & Moisture Gain

ANALYTICAL WORK PERFORMED, METHOD OF ANALYSIS, AND RESULTS
Particulates by SCAQMD Method 5.1L; Moisture gain by SCAQMD Method 4.1L

Received impinger volume, mL	208
Impinger gain, mL	8
Silica gel gain, g	7
Recovered volume, mL	900
Organic extraction residue, mg	<1
Insoluble residue, mg	1
Soluble residue, mg	3
Acid, as $H_2SO_4 \cdot 2H_2O$, mg	<1
Sulfates, as $H_2SO_4 \cdot 2H_2O$, mg	<1
Filter catch, mg	<1
Acid, as $H_2SO_4 \cdot 2H_2O$, mg	NR
Sulfates, as $H_2SO_4 \cdot 2H_2O$, mg	NR

NR) Not Requested

Approved By:

Margil W. Wadley
Margil W. Wadley, Ph.D.

Manager of Laboratory Services

TSD RECEIVED

AUG 18 1987

S.T. BRANCH

Truesdail Laboratories, Inc.

Source test of:

Gresham, Varner, Savage *(Plate)*
600 North Arrowhead Avenue
San Bernardino, California 92401

Laboratory No. 17468

UNACCEPTABLE

This report is unacceptable. The isokinetic sampling rate for both the inlet and outlet lies outside the plus or minus 10 percent that is allowable. Other discrepancies follow.

The moisture content in the stack gas is above saturation at both the inlet and outlet locations. Moisture contents given in the report cannot exist at the stack temperatures and pressures specified. The report gives a higher moisture at the scrubber inlet than at the outlet. This looks suspicious.

The report does not contain a good description of the train. There is no mention of the number of impingers or whether or not a silica gel impinger was used. The calculation of moisture in the report is strange. One of the values determined is the volume of water going through the gas meter. If the train contained a silica gel impinger, no moisture would have reached the dry gas meter. At any rate, the moisture content should not exceed saturation.

There is no meter box Y value given in the report, nor are there any dry gas meter calibration sheets. It is assumed that the train used in this report is an isokinetic train and almost identical to a Method 5 train.

It appears that the nozzles were not checked with a micrometer.

3/1/89

MEMORANDUM

SUBJECT: Acceptability of Test Reports for use as a Data Base for
Chromium NESHAP

FROM: Frank R. Clay

TO: Dallas Safriet
Pollutant Characterization Section (MD-15)

I have reviewed the following four test reports and have found them unacceptable for use in the Data Base for the Chromium NESHAP. The reasons that the reports are unacceptable are also given.

The reports have been returned to Andy Smith.

cc: Andy Smith

TRUESDAIL LABORATORY

CHEMISTS - MICROBIOLOGISTS
RESEARCH - DEVELOPMENT

CLIENT Gresham, Varner,
600 N. Arrowhead
San Bernardino, CA
Attention: James

SAMPLE Inlet & Outlet of
Line at Plato Products

INVESTIGATION

F. Clay

Please review,

Truesdail Report #17468

Plato Products

For D. Salfreit

Andy

2/22/89

INUE
680
6239
1564
88

87

87

Total and Hexavalent Chromium, Lead

SEP 05 1987

PLATO-CALIF.

RESULTS

On July 29, 1987, representatives of Truesdail Laboratories, Inc. conducted tests to determine the lead, hexavalent chromium and total chromium emissions at the inlet and outlet of a scrubber serving the parts plating line at the Plato Products facility in Glendora, California. In addition, the same measurements were taken of the background air at the property line upwind of the facility (northwest corner).

For each test location, the measurements were all taken with a single sampling train by collecting an 8-hour sample by the SCAQMD wet impingement method (5.1). The sampling trains consisted of a glass sampling probe connected with Teflon tubing to a set of Greenburg-Smith impingers charged with 200 mls of distilled water and followed by a glass fiber backup filter, a vacuum pump and a dry gas meter. The scrubber samples were collected isokinetically for 30 minutes at each of 16 traverse points.

The flue gas flow rate was determined at each scrubber test location prior to sampling by measuring the average velocity head with a Standard Pitot tube and a Magnehelic differential pressure gage, and by measuring the average temperature with a Chromel-Alumel thermocouple and a Micromite potentiometer.

The sample solutions were stabilized and refrigerated upon return to the laboratories, and subsequently analyzed along with the sample filters for total chromium and lead by atomic absorption spectroscopy and for hexavalent chromium by the diphenylcarbazide colorimetric method.

The results were as follows:

This report applies only to the sample, or samples, investigated and is not necessarily indicative of the quality or condition of apparently identical or similar products. As a mutual protection to clients, the public and these Laboratories, this report is submitted and accepted for the exclusive use of the client to whom it is addressed and upon the condition that it is not to be used, in whole or in part, in any advertising or publicity matter without prior written authorization from these Laboratories.

PLATO PRODUCTS
Laboratory Number 17468
07-29-87

<u>Flue Gas:</u>	<u>SCRUBBER Inlet</u>	<u>SCRUBBER Outlet</u>
Temperature, °F	73	68
Static Pressure, in. H ₂ O	-0.76	+0.01
Velocity, ft/sec	37.2	28.2
Flue Dimensions, in.	16	16
Flue Area, sq. ft.	1.40	1.40
Flow Rate, ACFM	3,127	2,416
, SCFM	2,937	2,375
, DSCFM	2,805	2,325
Moisture, % by vol.	4.5	2.9
 <u>Chromium</u>		
Sampling Time:	(06:35-14:55)	(06:35-14:52)
Sample Volume, DSCF	322.92	267.63
Concentration, ppm		
Total Cr	0.0036	0.0013
Cr+6	<0.0002	<0.0003
Concentrations, mg/m ³		
Total Cr	0.0076	0.0028
Cr+6	<0.00004	<0.00006
Emission Rate, lbs/hr		
Total Cr	0.00008	0.00002
Cr+6	<0.000005	<0.000006
 <u>Lead:</u>		
Sampling Time:	(06:35-14:55)	(06:35-14:52)
Sample Volume, DSCF	322.92	267.63
Concentrations		
Pb, ppm	<0.0002	<0.0003
, mg/m ³	<0.0016	<0.0022
Emission Rate, lbs/hr	<0.00002	<0.00002

TRUESDAIL LABORATORIES, INC.

PLATO PRODUCTS
Laboratory Number 17468
07-29-87

Chromium

Ambient
Northwest Boundry

Sampling Time:
Sample Volume, DSCF
Concentration, ppm
 Total Cr
 Cr+6
Concentrations, mg/m³
 Total Cr
 Cr+6

(06:38 - 15:10)
361.69

0.0003
<0.0003

0.0007
<0.0003

Lead:

Sampling Time:
Sample Volume, DSCF
Concentrations
 Pb, ppm
 , mg/m³

(06:38 - 15:10)
361.69

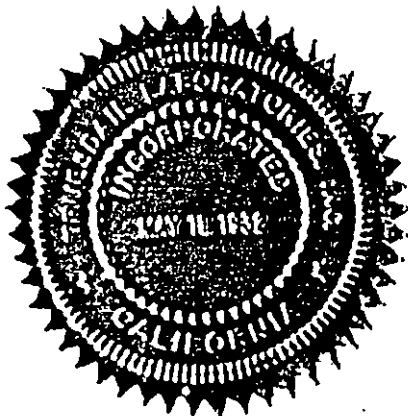
0.0002
0.0016

Respectfully submitted,

TRUESDAIL LABORATORIES, INC.

S. Hugh Brown

S. Hugh Brown, Supervisor
Air Pollution Testing



APPENDIX

Barometric Pressure: 25.84

$$L. \text{ FLOW RATE, } K \times \frac{520}{460 + J} \times \frac{BP + Ps/13.6}{29.9}, \text{ SCFM} \quad 2937$$

E-INK

SCR -
PUSPANTI 100GALS
WATER / HR

16"

TRUESDAIL LABORATORIES, INC.

Sampling Location: INLET - PLATO
Test No.

Date: 2/29/84
Barometric Pressure: 28.84
Nozzle Diameter: .25

Time	Gas Meter				Sample Point	CFM	15 ft. 30 ft.	36 in. cu. ft. 28.84	T
	Reading cu. ft. Vm	Press. in. H ₂ O Pm	Temp. of Tm	Impinger Temp. of T1					
705	164.70	1.0	72°	39°F	2	.84			
705	191.50	1.0	74°	39°F	2	.84			
735	216.25	.88	77°	42°F	3	.78			
7805	240.36	.70	80°	42°F	4	.74	1		
7835	262.16	.70	80°	42°F	5	.74			
0005	284.26	.71	80°	42°	6	.75			
0935	306.76	.58	80°	42°	7	.66			
1005	326.30	.55	80°	42°	7	.66			
1035	344.16								
1045	344.16	.70	80°	39°	2	.73			
1115	361.86	.66	80°	42°	2	.73	75		
1145	383.34	.65	82°	42°	3	.70			
1215	410.08	.65	84°	43°	4	.70			
1245	431.44	.70	84°	45°	5	.74	1250	Back Lost	
1325	452.64	.71	86°	46°	6	.75	333.80		
1355	475.26	.90	88°	46°	7	.81	1300		
1425	501.08	.90	90°	46°	7	.81			
1455	525.50	.75	81°	42°					

Weight Collected grams
360.80

METER #10
DATE 2/29/84

MF = 97
K = .9378

C = .65
H = .84
524.7
265
82
355
10/885

- A. Total Weight _____
- B. Condensate Volume, ml. 63ml
- C. Condensate Vapor Volume, $0.00267 \times \frac{460 + T_m}{B.P. + P_m/13.6} \times B$, cu. ft. 3.16
- D. Total Sample Volume, $V_m + C$, cu. ft. 363.96
- E. Sample Volume, $D \times \frac{520}{460 + T_m} \times \frac{28.90}{29.9} \times \frac{.955}{B.P. + P_m/13.6} \times \text{Moisture corr., DSCF}$ 322.92
- F. Concentration, $15.43 \times A/E$, grains/DSCF _____
- G. Stack Gas Flow Rate, DSCFM 2805
- H. Emissions, $60 \times G \times F/7000$, lbs/hr _____

Sampling Station PLATD - INLET Date 7/30/87

WATER VAPOR AND GAS DENSITY CALCULATIONS

Percent Water Vapor in Gases

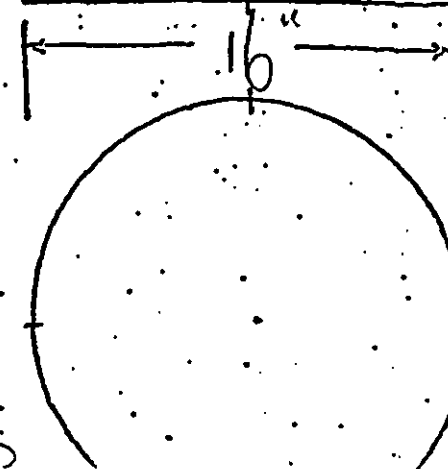
- A. Gas pressure at meter, in. Hg. (absolute) 28.78
- B. Vapor pressure of water at impinger temp., in. Hg. 1.066
- C. Volume of metered gas, cu. ft. 360.80
- D. Volume of water vapor metered, B X C/A, cu. ft. 13.36
- E. Volume of water vapor condensed, cu. ft. 3.16
- F. Total volume water vapor in gas sample, D + E, cu. ft. 16.52
- G. Total volume of gas sample, C + E, cu. ft. 363.96
- H. Percent water vapor in sampled gas, 100 x F/G 4.54

GAS DENSITY CORRECTION FACTOR

Component	Volume Percent/100 x Moisture Correction x Mol. Wt. =	Wt./Mole Wet Basis
Water	.045	18.0
Carbon Dioxide	Dry Basis	44.0
Carbon Monoxide	Dry Basis	28.0
Oxygen	Dry Basis	32.0
Nitrogen & Inerts	Dry Basis	28.2
Average Molecular Weight		

J. Density of gas referred to air = $\frac{\text{Av. Mol. Wt.}}{28.95} =$ _____

K. Gas density correction factor = $\sqrt{\frac{1.00}{J}} =$ _____



TRUESDAIL LABORATORIES, INC.

 Sampling Location: OUTLET - PWK
 Test No. 3

 Date: 7/21/87
 Barometric Pressure: 28.84
 Nozzle Diameter: .25

PC

Time	Gas Meter			Impinger Temp. OF T _i	Sample Point	CFM			
	Reading cu. ft. V _m	Press. in. H ₂ O P _m	Temp. OF T _m						
635	803.48	.46	72°	—	2	.59			
705	821.18	.49	72°	43°	2	.59			
735	839.62	.46	76°	47°	3	.60			
805	857.98	.46	70°	48°	4	.60			
835	876.00	.47	74°	53°	5	.61			
905	894.12	.47	78°	53°	6	.61			
935	912.34	.46	82°	56°	7	.59			
1005	930.61	.46	85°	56°	7	.59			
1035	949.04			59°					
1041	949.09	.47	90°	—	2	.61	CHANGE PORTS		
1111	968.16	.47	91°	59°	2	.61			
1141	986.24	.49	93°	59°	3	.63			
1211	1004.36	.48	95°	60°	4	.62			
1241	1022.79	.48	96°	61°	5	.62	8 min. into point power reduction of system & train resumed after 11 min.		
1322	1041.44	.46	98°	61°	6	.60			
1352	1060.30	.46	101°	58°	7	.60			
1422	1079.16	.45	102°	60°	7	.58			
1452	1096.82			60°					
Weight Collected, grams									
893.34		.47	96	56					

METER # 006

TARE WT = .1082

 L = .9569 MF = .97
 L = .57
 H = .60

- A. Total Weight 78.29
- B. Condensate Volume, ml. 78 ml
- C. Condensate Vapor Volume, $0.00267 \times \frac{460 + T_m}{B.P. + P_m/13.6} \times B$, cu. ft. 3.94
- D. Total Sample Volume, $V_m + C$, cu. ft. 297.28
- E. Sample Volume, $D \times \frac{520}{460 + T_m} \times \frac{28.87}{29.9} \times \frac{.979}{B.P. + P_m/13.6} \times \text{Moisture corr., DSCF}$ 267.63
- F. Concentration, $15.43 \times A/E$, grains/DSCF _____
- G. Stack Gas Flow Rate, DSCFM 2325
- H. Emissions, $60 \times G \times F/7000$, lbs/hr _____

Sampling Station PLATO - OUTLET Date 7/31/87

WATER VAPOR AND GAS DENSITY CALCULATIONS

Percent Water Vapor in Gases

- A. Gas pressure at meter, in. Hg. (absolute) 28.84
- B. Vapor pressure of water at impinger temp., in. Hg. .4520
- C. Volume of metered gas, cu. ft. 273.34
- D. Volume of water vapor metered, B X C/A, cu. ft. 4.60
- E. Volume of water vapor condensed, cu. ft. 3.94
- F. Total volume water vapor in gas sample, D + E, cu. ft. 8.54
- G. Total volume of gas sample, C + E, cu. ft. 277.28
- H. Percent water vapor in sampled gas, 100 x F/G 2.87

GAS DENSITY CORRECTION FACTOR

Component	Volume Percent/100 x Moisture Correction x Mol. Wt. = Wet Basis	Wt./Mole
Water	.029	18.0
Carbon Dioxide	Dry Basis	44.0
Carbon Monoxide	Dry Basis	28.0
Oxygen	Dry Basis	32.0
Nitrogen & Inerts	Dry Basis	28.2
Average Molecular Weight		

J. Density of gas referred to air = $\frac{\text{Av. Mol. Wt.}}{28.95} =$ _____

K. Gas density correction factor = $\sqrt{\frac{1.00}{J}} =$ _____

Sampling Location: PLATO
Test No. AMBIENT AIR

Date: 7/27/87
Barometric Pressure: 28.84
Nozzle Diameter:

(15)

Time	Gas Meter				Sample Point	CFM			
	Reading cu. ft. Vm	Press. in. H ₂ O Pm	Temp. OF Tm	Impinger Temp. OF Ti					
6:38	755.02		60°	10°					
7:08	778.72		64°	10°					
7:38	802.41		72°	10°					
8:08	826.68		78°	10°					
8:38	850.90		82°	10°					
9:08	875.24		86°	10°					
9:38	898.46		90°	10°					
10:08	923.35		93°	10°					
10:38	946.88		96°	10°					
11:08	970.70		98°	10°					
11:38	994.18		100°	11°					
12:08	1017.58		102°	10°					
12:38	1045.68		104°	10°	12:50				
1:10	1067.76		106°	10°	POWER BREAK FOR 2 MINUTES				
1:40	1090.64		107°	10°					
2:10	1114.52		107°	10°					
2:40	1138.60		107°	10°					
3:10	1157.31	.84	91°	10°					
Weight Collected		grams							
402.29									

METER #4 TARE 01288

- Total Weight _____
- Condensate Volume, ml. 62 ml
- Condensate Vapor Volume, $0.00267 \times \frac{460 + T_m}{B.P. + P_m/13.6} \times B$, cu. ft. 3.16
- Total Sample Volume, $V_m + C$, cu. ft. 405.45
- Sample Volume, $D \times \frac{520}{460 + T_m} \times \frac{B.P. + P_m/13.6}{29.9} \times \text{Moisture corr., DSCF}$ 361.69
- Concentration, $15.43 \times A/E$, grains/DSCF _____
- Stack Gas Flow Rate, DSCFM _____
- Emissions, $60 \times G \times F/7000$, lbs/hr _____

Sampling Station RATD - AMBIENT Date 8/3/87

WATER VAPOR AND GAS DENSITY CALCULATIONS

Percent Water Vapor in Gases

- A. Gas pressure at meter, in. Hg. (absolute) 28.90
- B. Vapor pressure of water at impinger temp., in. Hg. .3626
- C. Volume of metered gas, cu. ft. 402.29
- D. Volume of water vapor metered, B X C/A, cu. ft. 5.05
- E. Volume of water vapor condensed, cu. ft. 3.16
- F. Total volume water vapor in gas sample, D + E, cu. ft. 8.21
- G. Total volume of gas sample, C + E, cu. ft. 405.45
- H. Percent water vapor in sampled gas, 100 x F/G 2.02

GAS DENSITY CORRECTION FACTOR

Component	Volume Percent/100 x Moisture Correction x Mol. Wt. = Wet Basis			Wt./Mole
Water	.020	1.0	18.0	
Carbon Dioxide	Dry Basis	.980	44.0	
Carbon Monoxide	Dry Basis	↓	28.0	
Oxygen	Dry Basis		32.0	
Nitrogen & Inerts	Dry Basis		28.2	

Average Molecular Weight

J. Density of gas referred to air = $\frac{\text{Av. Mol. Wt.}}{28.95}$ =

K. Gas density correction factor = $\sqrt{\frac{1.00}{J}}$ =

Total Cr (ppm)

- SOLUTIONS

Gresham, Varner, Savage (Plato)

TLET

$$.05 \text{ ppm Cr} = .05 \text{ mg/l} \times \frac{1000 \text{ mg}}{1 \text{ mg}}$$

$$.05 \text{ mg/l} \times .425 \text{ l} \times \frac{1 \text{ mole Cr}}{52 \text{ mg Cr}} \times \frac{23.7 \text{ ml}}{1 \text{ mole Cr}} \times \frac{1000 \text{ ul}}{1 \text{ ml}} \times \frac{10 \text{ scF}}{28.32 \text{ l}} \times \frac{1}{267.63 \text{ DscF}}$$

$$= .0013 \text{ ppm (v) Cr}$$

NLET

$$.19 \text{ ppm Cr} = .19 \text{ mg/l}$$

$$.19 \text{ mg/l} \times .365 \text{ l} \times \frac{1 \text{ mole Cr}}{52 \text{ mg Cr}} \times \frac{23.7 \text{ ml}}{1 \text{ mole Cr}} \times \frac{1000 \text{ ul}}{1 \text{ ml}} \times \frac{10 \text{ scF}}{28.32 \text{ l}} \times \frac{1}{322.92 \text{ DscF}}$$

$$= .0035 \text{ (v) Cr}$$

AMBIENT AIR

$$.02 \text{ ppm Cr} = .02 \text{ mg/l}$$

$$.02 \text{ mg/l} \times .335 \text{ l} \times \frac{1 \text{ mole Cr}}{52 \text{ mg Cr}} \times \frac{23.7 \text{ ml}}{1 \text{ mole Cr}} \times \frac{1000 \text{ ul}}{1 \text{ ml}} \times \frac{10 \text{ scF}}{28.32 \text{ l}} \times \frac{1}{367.69 \text{ DscF}}$$

$$= .0003 \text{ ppm (v) Cr}$$

Total Cr (ppm)
Filters
Gresham, Varner, Savage (Pluto)

OUTLET

$$< 1.00 \text{ mg} = .001 \text{ mg}$$

$$.001 \text{ mg} \times \frac{1 \text{ mmole Cr}}{52 \text{ mg Cr}} \times \frac{23.7 \text{ ml}}{1 \text{ mmole}} \times \frac{1000 \text{ ul}}{1 \text{ ml}} \times \frac{10 \text{ SCF}}{28.32 \text{ lb}} \times \frac{1}{267.63 \text{ DSCF}}$$

$$= \boxed{< .0001 \text{ ppm (V) Cr}}$$

NLET

$$1.14 \text{ mg} = .001 \text{ mg}$$

$$.001 \text{ mg} \times \frac{1 \text{ mmole Cr}}{52 \text{ mg Cr}} \times \frac{23.7 \text{ ml}}{1 \text{ mmole}} \times \frac{1000 \text{ ul}}{1 \text{ ml}} \times \frac{10 \text{ SCF}}{28.32 \text{ lb}} \times \frac{1}{322.92 \text{ DSCF}}$$

$$= \boxed{0.0001 \text{ ppm (V) Cr}}$$

IMBIENT AIR

$$< 1.00 \text{ mg} = .001 \text{ mg}$$

$$.001 \text{ mg} \times \frac{1 \text{ mmole Cr}}{52 \text{ mg Cr}} \times \frac{23.7 \text{ ml}}{1 \text{ mmole}} \times \frac{1000 \text{ ul}}{1 \text{ ml}} \times \frac{10 \text{ SCF}}{28.32 \text{ lb}} \times \frac{1}{361.69 \text{ DSCF}}$$

$$= \boxed{< .6001 \text{ ppm (V) Cr}}$$

Total Cr (mg/m^3) $1 \text{ m}^3 = 1000 \text{ l}$

SOLUTIONS

Gresham, Varner, Savage (Plato)

OUTLET

$$0.05 \text{ ppm Cr} = \text{mg/l} = \text{mg}/\text{m}^3$$

$$\frac{0.05 \text{ mg}}{\text{l}} \times 0.425 \text{ l} \times \frac{\text{DSCF}}{28.3 \text{ l}} \times \frac{1}{267.63 \text{ DSCF}} \times \frac{1000 \text{ l}}{1 \text{ m}^3}$$

$$\text{mg}/\text{m}^3 = \boxed{0.0028 \text{ mg}/\text{m}^3 \text{ Cr}}$$

INLET

$$.19 \text{ ppm Cr} = .19 \text{ mg/l}$$

$$\frac{19 \text{ mg}}{\text{l}} \times .365 \text{ l} \times \frac{\text{DSCF}}{28.3 \text{ l}} \times \frac{1}{322.92 \text{ DSCF}} \times \frac{1000 \text{ l}}{1 \text{ m}^3}$$

$$= \boxed{0.0076 \text{ mg}/\text{m}^3 \text{ Cr}}$$

AMBIENT AIR

$$.02 \text{ ppm Cr} = .02 \text{ mg/l}$$

$$\frac{.02 \text{ mg}}{\text{l}} \times .335 \text{ l} \times \frac{\text{DSCF}}{28.3 \text{ l}} \times \frac{1}{361.69 \text{ DSCF}} \times \frac{1000 \text{ l}}{1 \text{ m}^3}$$

$$= \boxed{.0007 \text{ mg}/\text{m}^3 \text{ Cr}}$$

Total Cr (mg/m^3)
Filters

Gresham, Varner, Savage (Plato)

OUTLET

$$< 1.60 \text{ mg} = .001 \text{ mg}$$

$$.001 \text{ mg} \times \frac{\text{DSCF}}{28.3 \text{ l}} \times \frac{1}{267.63 \text{ DSCF}} \times \frac{1000 \text{ l}}{1 \text{ m}^3}$$

$$= 0.0004 \text{ mg}/\text{m}^3 \text{ Cr}$$

INLET

$$1.14 \text{ mg} = .001 \text{ mg}$$

$$.001 \text{ mg} \times \frac{\text{DSCF}}{28.3 \text{ l}} \times \frac{1}{322.92 \text{ DSCF}} \times \frac{1000 \text{ l}}{1 \text{ m}^3}$$

$$= 0.0004 \text{ mg}/\text{m}^3 \text{ Cr}$$

AMBIENT AIR

$$< 1.60 \text{ mg} = .001 \text{ mg}$$

$$.001 \text{ mg} \times \frac{\text{DSCF}}{28.3 \text{ l}} \times \frac{1}{361.69 \text{ DSCF}} \times \frac{1000 \text{ l}}{1 \text{ m}^3}$$

$$= 0.0001 \text{ mg}/\text{m}^3 \text{ Cr}$$

Cr^{+6} (ppm)
SOLUTIONS

Gresham, Varner, Savage (Plato)

PLET

$$< 0.01 \text{ ppm } \text{Cr}^{+6} = .01 \text{ mg/l}$$

$$\cancel{.01 \text{ mg}} / \cancel{\text{l}} \times .425 \text{ l} \times \frac{1 \text{ mole Cr}}{52 \text{ mg Cr}} \times \frac{23.3 \text{ ml}}{1 \text{ mmole Cr}} \times \frac{1000 \text{ ml}}{1 \text{ ml}} \times \frac{10 \text{ SCF}}{28.32 \text{ l}} \times \frac{1}{267.63 \text{ DSCF}}$$

$$= < .0003 \text{ ppm (v) } \text{Cr}^{+6}$$

NLET

$$< 0.01 \text{ ppm } \text{Cr}^{+6} = .01 \text{ mg/l}$$

$$.01 \text{ mg/l} \times .365 \text{ l} \times \frac{1 \text{ mmole Cr}}{52 \text{ mg Cr}} \times \frac{23.3 \text{ ml}}{1 \text{ mmole Cr}} \times \frac{1000 \text{ ml}}{1 \text{ ml}} \times \frac{10 \text{ SCF}}{28.32} \times \frac{1}{322.92 \text{ DSCF}}$$

$$= < .0002 \text{ ppm (v) } \text{Cr}^{+6}$$

AMBIENT AIR

$$< 0.01 \text{ ppm } \text{Cr}^{+6} = .01 \text{ mg/l}$$

$$.01 \text{ mg/l} \times .335 \text{ l} \times \frac{1 \text{ mmole Cr}}{52 \text{ mg Cr}} \times \frac{23.3 \text{ ml}}{1 \text{ mmole Cr}} \times \frac{1000 \text{ ml}}{1 \text{ ml}} \times \frac{10 \text{ SCF}}{28.32} \times \frac{1}{361.69 \text{ DSCF}}$$

$$= < .0002 \text{ ppm (v) } \text{Cr}^{+6}$$

Cr⁶⁺ (ppm)
Filters

Gresham, Varner, Savage (Plato)

UTLET

$$< 0.01 \text{ ppm Cr}^{6+} = .01 \text{ mg/l}$$

$$.01 \text{ mg/l} \times \frac{0.1}{.425} \times \frac{1 \text{ mole Cr}}{52 \text{ mg Cr}} \times \frac{23.3 \text{ ml}}{1 \text{ mmole Cr}} \times \frac{1000 \text{ ml}}{1 \text{ ml}} \times \frac{10 \text{ SCF}}{28.32} \times \frac{1}{267.63 \text{ DSCF}}$$

$$= < .0001 \text{ ppm (V) Cr}^{6+}$$

NLET

$$< 0.01 \text{ ppm Cr}^{6+} = .01 \text{ mg/l}$$

$$.01 \text{ mg/l} \times \frac{0.1}{.365} \times \frac{1 \text{ mmole Cr}}{52 \text{ mg Cr}} \times \frac{23.7 \text{ ml}}{1 \text{ mmole}} \times \frac{1000 \text{ ml}}{1 \text{ ml}} \times \frac{10 \text{ SCF}}{28.32} \times \frac{1}{322.92 \text{ DSCF}}$$

$$= < .0001 \text{ ppm (V) Cr}^{6+}$$

AMBIENT AIR

$$< 0.01 \text{ ppm Cr}^{6+} = .01 \text{ mg/l}$$

$$.01 \text{ mg/l} \times \frac{0.1}{.335} \times \frac{1 \text{ mmole Cr}}{52 \text{ mg Cr}} \times \frac{23.7 \text{ ml}}{1 \text{ mmole}} \times \frac{1000 \text{ ml}}{1 \text{ ml}} \times \frac{10 \text{ SCF}}{28.32} \times \frac{1}{361.69 \text{ DSCF}}$$

$$= < .0001 \text{ ppm (V) Cr}^{6+}$$

$\text{Cr}^{+6} (\text{mg}/\text{m}^3)$

SOLUTIONS

Gresham, Varner, Savage (Plato)

OUTLET

$$< 0.01 \text{ ppm } \text{Cr}^{+6} = .01 \text{ mg/l}$$

$$.01 \text{ mg/l} \times 0.425 \text{ l} \times \frac{\text{DSCF}}{28.3} \times \frac{1}{267.63 \text{ DSCF}} \times \frac{1000 \text{ l}}{1 \text{ m}^3}$$

$$= < .0006 \text{ mg}/\text{m}^3$$

INLET

$$< 0.01 \text{ ppm } \text{Cr}^{+6} = .01 \text{ mg/l}$$

$$.01 \text{ mg/l} \times 1.365 \text{ l} \times \frac{\text{DSCF}}{28.3 \text{ l}} \times \frac{1}{322.92 \text{ DSCF}} \times \frac{1000 \text{ l}}{1 \text{ m}^3}$$

$$= < .0004 \text{ mg}/\text{m}^3$$

AMBIENT AIR

$$< 0.01 \text{ ppm } \text{Cr}^{+6} = .01 \text{ mg/l}$$

$$.01 \text{ mg/l} \times .335 \text{ l} \times \frac{\text{DSCF}}{28.3 \text{ l}} \times \frac{1}{361.69 \text{ DSCF}} \times \frac{1000 \text{ l}}{1 \text{ m}^3}$$

$$= < .0003 \text{ mg}/\text{m}^3$$

$$Cr^{+6} (mg/m^3)$$

Filters

Gresham, Varner, Savage (Plato)

OUTLET

$$20.01 \text{ ppm } Cr^{+6} = .01 \text{ mg/l}$$

$$.01 \text{ mg/l} \times \frac{0.1}{28.3 \text{ l}} \times \frac{DSCF}{257.63 \text{ DSCF}} \times \frac{1}{1} \times \frac{1000 \text{ l}}{1 \text{ m}^3}$$

$$= \boxed{.0001 \text{ mg/m}^3}$$

INLET

$$20.01 \text{ ppm } Cr^{+6} = .01 \text{ mg/l}$$

$$.01 \text{ mg/l} \times \frac{0.1}{28.3 \text{ l}} \times \frac{DSCF}{322.92 \text{ DSCF}} \times \frac{1}{1} \times \frac{1000 \text{ l}}{1 \text{ m}^3}$$

$$= \boxed{.0001 \text{ mg/m}^3}$$

AMBIENT AIR

$$< 0.01 \text{ ppm } Cr^{+6} = .01 \text{ mg/l}$$

$$.01 \text{ mg/l} \times \frac{0.1}{28.3 \text{ l}} \times \frac{DSCF}{361.69 \text{ DSCF}} \times \frac{1}{1} \times \frac{1000 \text{ l}}{1 \text{ m}^3}$$

$$= \boxed{.0001 \text{ mg/m}^3}$$

Pb (-PPM)

INLET

$$0.04 \text{ PPM} = 0.04 \text{ mg/l} \sim \text{ul/l}$$

$$0.04 \frac{\text{mg}}{\text{l}} \times 0.365 \text{ l} \times \frac{1 \text{ mmole Pb}}{207.2 \text{ mg Pb}} \times 23.7 \text{ ml} \times \frac{1000 \text{ ul}}{1 \text{ ml}} \times \frac{\text{DSCF}}{28.3 \text{ l}} \times \frac{1}{322.92 \text{ DSCF}}$$

$$= \boxed{0.0002 \text{ ul/l} = \text{PPM(V) Pb}}$$

OUTLET

$$0.04 \text{ PPM} = 0.04 \text{ mg/l} \sim \text{ul/l}$$

$$0.04 \frac{\text{mg}}{\text{l}} \times 0.425 \text{ l} \times \frac{1 \text{ mmole Pb}}{207.2 \text{ mg Pb}} \times 23.7 \text{ ml} \times \frac{1000 \text{ ul}}{1 \text{ ml}} \times \frac{\text{DSCF}}{28.3 \text{ l}} \times \frac{1}{267.63 \text{ DSCF}}$$

$$= \boxed{0.0003 \text{ ul/l} = \text{PPM(V) Pb}}$$

AMBIENT

$$0.05 \text{ PPM} = 0.05 \text{ mg/l} \sim \text{ul/l}$$

$$0.05 \frac{\text{mg}}{\text{l}} \times 0.335 \text{ l} \times \frac{1 \text{ mmole Pb}}{207.2 \text{ mg Pb}} \times 23.7 \text{ ml} \times \frac{1000 \text{ ul}}{1 \text{ ml}} \times \frac{\text{DSCF}}{28.3 \text{ l}} \times \frac{1}{361.69 \text{ DSCF}}$$

$$= \boxed{0.0002 \text{ ul/l} = \text{PPM(V) Pb}}$$

FILTERS

Pb (PPM)

INLET

$$4.12 \mu\text{g} = 0.00412 \text{ mg} \sim \frac{\mu\text{g}}{\text{L}}$$

$$\frac{0.00412 \text{ mg}}{207.2 \text{ mg}} \times \frac{1 \text{ mmole Pb}}{1 \text{ mmole Pb}} \times \frac{23.7 \text{ mL}}{1 \text{ mL}} \times \frac{1000 \mu\text{L}}{28.3 \text{ L}} \times \frac{\text{DSCF}}{322.92 \text{ DSCF}} \times 1$$

$$= \boxed{0.00005 \frac{\mu\text{g}}{\text{L}} = \text{PPM(V) Pb}}$$

OUTLET

$$< 2.00 \mu\text{g} = 0.002 \text{ mg} \sim \frac{\mu\text{g}}{\text{L}}$$

$$\frac{0.002 \text{ mg}}{207.2 \text{ mg}} \times \frac{1 \text{ mmole Pb}}{1 \text{ mmole Pb}} \times \frac{23.7 \text{ mL}}{1 \text{ mL}} \times \frac{1000 \mu\text{L}}{28.3 \text{ L}} \times \frac{\text{DSCF}}{267.63 \text{ DSCF}} \times 1$$

$$= \boxed{0.00003 \frac{\mu\text{g}}{\text{L}} = \text{PPM(V) Pb}}$$

AMBIENT

$$< 2.00 \mu\text{g} = 0.002 \text{ mg} \sim \frac{\mu\text{g}}{\text{L}}$$

$$\frac{0.002 \text{ mg}}{207.2 \text{ mg}} \times \frac{1 \text{ mmole Pb}}{1 \text{ mmole Pb}} \times \frac{23.7 \text{ mL}}{1 \text{ mL}} \times \frac{1000 \mu\text{L}}{28.3 \text{ L}} \times \frac{\text{DSCF}}{361.69 \text{ DSCF}} \times 1$$

$$\boxed{< 0.00002 \frac{\mu\text{g}}{\text{L}} = \text{PPM(V) Pb}}$$

SOLUTIONS

Pb - mg/m^3

INLET

$$<0.04 \text{ ppm} = 0.04 \text{ mg/l}$$

$$\frac{0.04 \text{ mg}}{\text{l}} \times 0.365 \text{ l} \times \frac{\text{DSCF}}{28.3 \text{ l}} \times \frac{1}{377.92 \text{ DSCF}} \times \frac{1000 \text{ l}}{1 \text{ m}^3}$$

$$= \boxed{0.0016 \text{ mg}/\text{m}^3 \text{ Pb}}$$

OUTLET

$$<0.04 \text{ ppm} = 0.04 \text{ mg/l}$$

$$\frac{0.04 \text{ mg}}{\text{l}} \times 0.425 \text{ l} \times \frac{\text{DSCF}}{28.3 \text{ l}} \times \frac{1}{267.63 \text{ DSCF}} \times \frac{1000 \text{ l}}{1 \text{ m}^3}$$

$$= \boxed{0.0022 \text{ mg}/\text{m}^3 \text{ Pb}}$$

AMBIENT

$$0.05 \text{ ppm} = 0.05 \text{ mg/l}$$

$$\frac{0.05 \text{ mg}}{\text{l}} \times 0.335 \text{ l} \times \frac{\text{DSCF}}{28.3 \text{ l}} \times \frac{1}{361.69 \text{ DSCF}} \times \frac{1000 \text{ l}}{1 \text{ m}^3}$$

$$= \boxed{0.0016 \text{ mg}/\text{m}^3 \text{ Pb}}$$