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Background Report Reference

AP-42 Section Number: 12.20

Background Chapter: 4

Reference Number: 56

Title: Inlet and Outlet Scrubber Serving
Chrome Dip Tank, Particulate and
Chromium Removal Efficiencies

Truesdail Laboratories

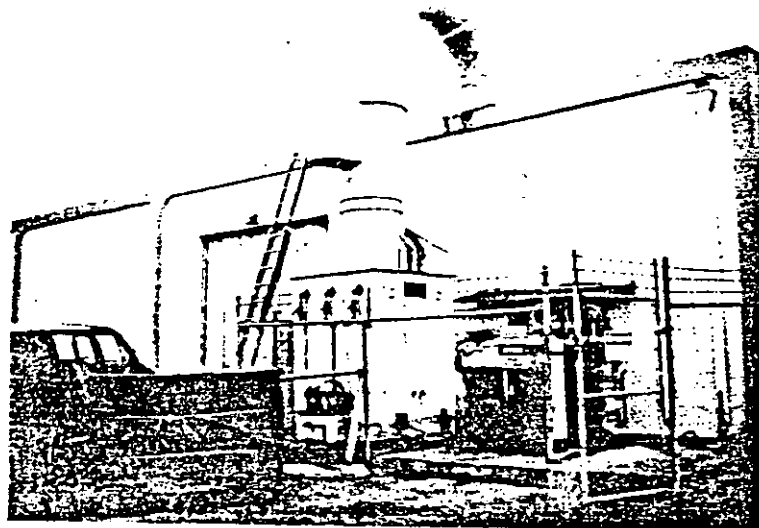
April 1986

South Coast Air Quality Management District

Field Report *Camion*

APPL. NO.

INSPECTION DATE



B. JOHN ATAIA
Air Quality Engineer

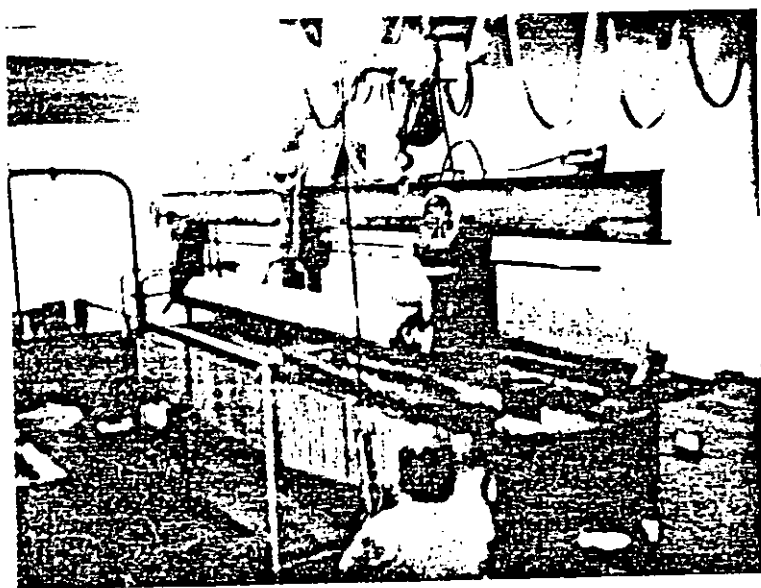
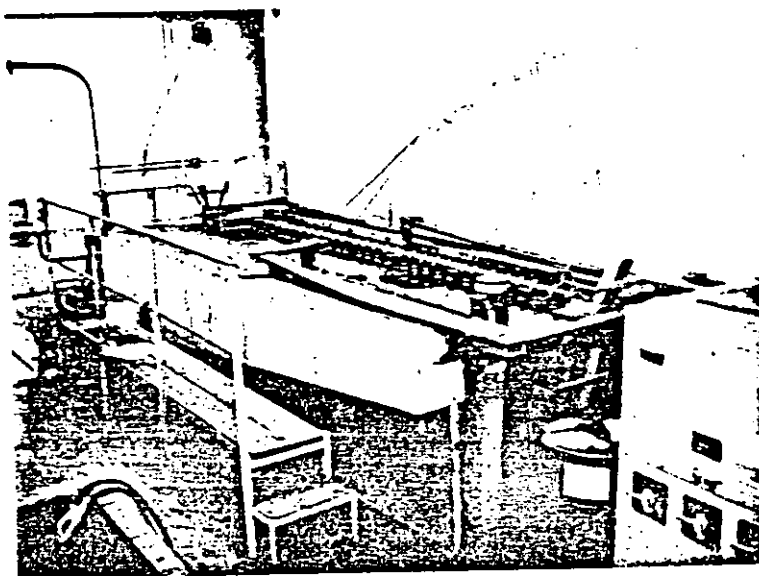
South Coast
Air Quality Management District
Engineering Division

9150 Flair Drive
El Monte, CA 91731
(916) 572-6180

(818)

SCRUBBER IS LOCATED
THIS WALL

CHROME TANK



DURING LOADING OF
A ROLLER

EMISSION FACTOR DETERMINATION
HARD CHROME PLATING TANK

REFERENCE: PAMARCO PACIFIC INC., APPLICATION NO. 133197
TRUESDAIL LAB. NO. 05789 (FEB. 6, 1986)

BASIC EQUIPMENT DESIGN & OPERATING DATA:

TANK DIMENSIONS: 3'-8"W. X 15'-0" L X 3'-6"D.

OPERATING TEM.: 135 F

SOLUTION : 50 OZ/GAL CHROMIC ACID

APPLIED POWER : 6V/2300A

INTERNAL CONTROL: FLOATS

CONTROL EQUIPMENT DESIGN & OPERATING DATA:

EQUIPMENT : VERTICAL PACKED TYPED WET SCRUBBER
WITH 9 NOZZLES, 5'-0"W. X 5'-0" L. X
2'-0"H., PACKING & 10" MESH TYPE
MIST ELIMINATOR.

TYPE OF PACKING : TRI-PACK NO. 2

VELOCITY : 500 FT/MIN

SCRUBBER DIMENSIONS: 5'-0"W. X 5'-0" L. X 8'-0"D.

EQUIVALENT DIAMETER: 5'-5"

RECIRCULATION RATE: 100 GPM

GAL/1000CFM: 10

THE SCRUBBER SUMP CAPACITY IS 180 GALLONS.

90 GALLONS OF SCRUBBING SOLUTION IS SENT TO THE
TANK ONCE DAY & A FRESH WATER IS ADDED TO THE
SCRUBBER **WITH NO OVERFLOW**

EMISSION FACTOR (UNCONTROLLED):

SOLID PARTICULATES : $(1.29 \text{ Lb/Hr}) / (55 \text{ SQ.FT.}) =$
0.023 Lb/Hr-SQ.FT.

CHROMIUM : $(0.009 \text{ Lb/Hr}) / (55$
 $\text{SQ.FT.}) = 0.00016 \text{ Lb/Hr-SQ.FT.}$

EMISSION FACTOR (CONTROLLED)

SOLID PARTICULATES: $(1.51 \text{ Lb/Hr}) / (55 \text{ SQ.FT.}) =$
0.027 Lb/Hr-SQ.FT.

CHROMIUM: $(0.005 \text{ Lb/Hr}) / (55 \text{ SQ.FT.}) =$
0.000091 Lb/Hr-SQ.FT.

PARTICULATE REMOVAL EFFICIENCY: (-17%)

CHROMIUM REMOVAL EFFICIENCY: 44.4%

REPORT

TRUESDAIL LABORATORIES, INC.

RECEIVED
ON 4/14/86IT WAS HANDLED TO ME
BY MR. STOCKINGCHEMISTS - MICROBIOLOGISTS - ENGINEERS
RESEARCH - DEVELOPMENT - TESTING14201 FRANKLIN AVENUE
TUSTIN, CALIFORNIA 92680
AREA CODE 714 • 730-6239
AREA CODE 213 • 225-1564
CABLE: TRU ELA B SCLIENT Dalco Engineering
15222 Los Flores
La Mirada, CA. 90638
ATTN: Dale Stocking

DATE April 11, 1986

RECEIVED February 4, 1986

SAMPLE Inlet and Outlet of Scrubber Serving Chrome Dip Tank
P.O. NO. 0313

LABORATORY NO. 05789

INVESTIGATION Particulate and Chromium Removal Efficiencies

RESULTS

On February 6, 1986 representatives of Truesdail Laboratories, Inc. conducted tests to determine the total particulate matter, total chromium (Cr^+), and hexavalent chromium (Cr^{++}) at the inlet and outlet of a scrubber serving the chrome dip tank at Pamarco Company in Orange, Calif.

The tests were conducted at both sampling locations ~~simultaneously~~ and the test period covered the entrance, exit, and 63-minute dip time of the part in the chrome tank. The scrubber discharged into a drum reservoir and sampling was conducted upstream of this point.

For each test location, the particulate matter was collected isokinetically for 3 minutes at each of 24 sampling points (12 on each diameter). The sampling train consisted of a glass probe connected with Teflon tubing to a set of Greenburg-Smith impingers charged with 200 mls of distilled water and followed by a glass fiber backup filter, a vacuum pump and a dry gas meter.

The flue gas flow rate was determined before the sampling traverse by measuring the average velocity head with either an S-type or a Standard Pitot tube and a Magnehelic differential pressure gage, and by measuring the average temperature with a Chromel-Alumel thermocouple and a Micromite potentiometer.

The particulate collections were filtered through their respective backup filters and aliquots of the filtrates were analyzed for total chromium by atomic absorption. The remaining filtrate portions were evaporated to dryness at 100°C and all sample residues were desiccated to a constant weight. No analysis for hexavalent chromium was made because the detection limit for this method was higher than the amount analyzed as total Cr^+ .

The location of the sampling holes at the scrubber inlet did not meet minimum requirements for velocity measurements. The velocity measurements obtained at this location were used only for isokinetic sampling rates. The flow rates calculated from these measurements disagreed with those of the outlet. Since the outlet location was the less turbulent of the two, all emission rates were calculated from outlet flow rates.

The results were as follows:

PAMARCO
2-6-86

Flue Gas

Scrubber Inlet

Scrubber Outlet

Temperature, °F
Static Pressure, In. H₂O
Velocity, Ft/Sec
Flue Dimensions, in.
Flue Area, sq. ft.
Flow Rate, ACFM
 , SCFM
 , DSCFM
Moisture, % by Vol.
Saturation, % by vol.

68
-1.4
34.7
21 x 36
5.25
(10,800)
(10,800)
(10,700)
1.3
2.3

61
-0.01
27.5
30
4.91
8110
8050
7900 -
1.9
1.8

Particulate Matter

Collection, Grams
 Filter
 Impingers
 Total
Sample Volume, DSCF
Concentration, grains/DSCF
Emission Rate, lbs/hr

Chromium (Cr⁺), mg/m³
 , lbs/hr

Particulate Removal, %
Chromium Removal, %

0.0000
0.0489
0.0489
39.50
0.0191
1.29*

0.30
0.009*

0.0001
0.0449
0.0450
31.07
0.0223
1.51

0.18
0.005

-17.1
44.4

* Calculated with Outlet Flow Rate.

Respectfully Submitted

TRUESDAIL LABORATORIES, INC.

S. Hugh Brown

S. Hugh Brown, Supervisor
Air Pollution Testing

HEXAVALENT

0.02 mg/m³

~~HEXAVALENT~~

TRUESDAIL LABORATORIES, INC.

APPENDIX

Barometric Pressure: 29

A. AVERAGE VELOCITY (TRAVERSE) ft/sec 34.67

B. REFERENCE POINT VELOCITY (TRAVERSE) ft/sec _____

C. AVERAGE VELOCITY (REFERENCE PT.) ft/sec _____

D. FLUE FACTOR C/B _____

E. PITOT TUBE CORRECTION FACTOR 0.83

F. GAS DENSITY CORRECTION FACTOR 1.001

G. CORRECTED VELOCITY, $A \times E \times F$, ft/sec 34.67
or, $A \times D \times E \times F$, ft/sec _____

H. AREA OF FLUE, SQ. FT. 5.25

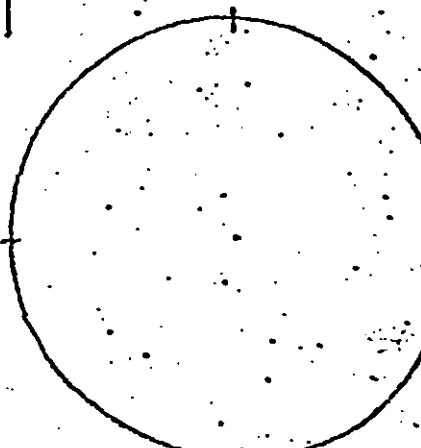
J. AVERAGE FLUE TEMPERATURE, °F 68

K. FLOW RATE, $G \times H \times 60$, CFM 12921

L. FLOW RATE, $K \times \frac{520}{460 + J} \times \frac{BP + Ps/13.6}{29.9}$, SCFM 10842

M. FLOW RATE, $L \times$ MOISTURE CORR., DSCFM 10701

← 3.6



Static Pressure, P_s : - 0.0

Test No.: Outlet.

Barometric Pressure: 29.7

[illegible]

A. AVERAGE VELOCITY (TRAVERSE) ft/sec 27.48

B. REFERENCE POINT VELOCITY (TRAVERSE) ft/sec _____

C. AVERAGE VELOCITY (REFERENCE PT.) ft/sec _____

D. FLUE FACTOR C/B _____

E. PITOT TUBE CORRECTION FACTOR STD 1.0

F. GAS DENSITY CORRECTION FACTOR 1.022

G. CORRECTED VELOCITY, $A \times E \times F$, ft/sec 27.5
or, $A \times D \times E \times F$, ft/sec

H. AREA OF FLUE, SQ. FT. _____ 7.97

J. AVERAGE FLUE TEMPERATURE, °F 61

K. FLOW RATE, $G \times H \times 60$, CFM _____ 8701

$$L. \text{ FLOW RATE, K} \times \frac{520}{460 + J} \times \frac{BP + Ps/13.6}{29.9}, \text{ SCFM} \quad 8050$$

M. FLOW RATE, L x MOISTURE CORR., DSCFM 790

09814

TRUESDAIL LABORATORIES, INC.

Lab. No. _____

EPA FIELD TEST DATA

Plant Dalco chrome

Sampling Station Inlet

Date 2-6-86

Flue Dimensions 36" X 21"

Test No. _____

Amb. Temp., °F _____

Bar. Pressure, In. Hg 29.73

Stack Pressure, In. H₂O -1.4

Sampling Nozzle Diam., In. 0.225

Pf .83

K = .7672

Sampling Apparatus No.: 540 10388

Trav. Point No.	Sampling Time	Sample Volume, Cu. Ft.	Vel. Head $\sqrt{Ps}$	Orifice ΔH In. H ₂ O	TEMPERATURE, °F				
					Stack	Probe CFM	Oven	Impinger Inlet	Gas Meter
1	10:36	516	.01	.05	66	.28		40	64
2	10:39	590	.01	.50	67	.72			64
3	10:42	790	.86	.72	68	.22			64
4	10:45	1050	.95	.75	68	.86		43	64
5	10:48	1308	.90	.72	68	.84			65
6	10:51	1560	.40	.37	68	.56			65
7	10:54	1748	.09	.15	68	.23		45	66
8	10:57	1828	0						
9	11:01	1828	.04	.04	66	.18		40	66
10	11:04	1899	.52	.44	67	.64			66
11	11:07	2092	.80	.66	67	.80			67
12	11:10	2336	.80	.66	68	.80		43	67
13	11:13	2540	1.0	.82	68	.84			68
14	11:16	2850	1.0	.87	68	.87			68
15	11:19	3120	.50	.43	68	.63		43	69
16	11:21	3314	0						
	11:24	3314							
17	11:24	3314	0						
18	11:27	3314	.34	.30	67	.52		40	69
19	11:30	3480	.65	.52	67	.72			70
20	11:33	3690	.50	.42	68	.63		43	70
21	11:36	3876	.45	.40	68	.60			70
22	11:39	4060	.50	.42	68	.63			70
23	11:42	4252	.67	.54	68	.71		45	71
24	11:45	4470	.15	.10	68	.25			71
	11:48	4577							
TOTAL		40.61							
AVG.			0.62	.46	68			43	67

Operator(s) CF

3m/cond

Barometric Pressure: 29.73

Nozzle Diameter: . 0.225

Weight Collected, grams

CR⁺ 0.30 mg/m³

Sampling Station DALCO - INLET Date 2-6-86

WATER VAPOR AND GAS DENSITY CALCULATIONS

Percent Water Vapor in Gases

- A. Gas pressure at meter, In. Hg. (Absolute) 29.76
- B. Vapor pressure of water at impinger temp., In. Hg. 0.2782
- C. Volume of metered gas, Cu. Ft. 40.61
- D. Volume of water vapor metered, B X C/A, Cu. Ft. 0.38
- E. Volume of water vapor condensed, Cu. Ft. 0.14
- F. Total volume of water vapor in gas sample, D+E, Cu. Ft. 0.52
- G. Total volume of gas sample, C+E, Cu. Ft. 40.75
- H. Percent water vapor in sampled gas, 100 X F/G 1.3

Gas Density Correction Factor

Component	Volume Percent/100 x Moisture Correction x Mol. Wt. =	Wt./Mole Wet Basis
Water	0.013	18.0
Carbon Dioxide	0.004 Dry Basis	44.0
Carbon Monoxide	Dry Basis	28.0
Oxygen	0.210 Dry Basis	32.0
Nitrogen & Inerts	0.786 Dry Basis	28.2

Average Molecular Weight 28.918

J. Density of gas referred to air = $\frac{\text{Av. Mol. Wt.}}{28.95}$ 0.9989

K. Gas density correction factor = $\sqrt{\frac{1.00}{J}}$ 1.001

Sampling Location:

DALCO

Barometric Pressure:

29.73

Test No.

Outlet Port 2

Nozzle Diameter:

0.225

Time	Gas Meter			Imping- er Temp °F T _i	CFM Sample Point	V ₄	T _s °		
	Reading cu. ft. V _m	Press. "H ₂ O P _m	Temp. °F T _m						
0	11:20	31.15	0.25	70	47	0.49	0.20	61	
3	11:23	32.62	"	70	48	"	0.20	"	
6	11:26	34.09	"	70	48	"	0.20	"	
9	11:29	35.56	"	"	49	"	0.20	"	
12	11:32	37.03	"	"	50	"	0.20	"	
15	11:35	38.50	"	69	51	0.46	0.18	"	
18	11:38	39.88	0.22	69	50	0.45	0.17	"	
21	11:41	41.23	0.21	70	50	0.43	0.16	"	
24	11:44	42.52	0.17	70	48	"	0.16	"	
27	11:47	43.81	0.17	70	46	"	0.16	"	
30	11:50	45.10	0.17	71	46	"	0.16	"	
33	11:53	46.39	0.16	71	"	0.42	0.15	"	
36	11:56	47.64	"	"	"				

Weight Collected, grams

Sheet 2

A. Total Weight

B. Condensate Volume, ml.

C. Condensate Vapor Volume, $0.00267 \times \frac{460 + T_m}{B.P. + P_m/13.6} \times B$, cu. ft.

D. Total Sample Volume, $V_m + C$, cu. ft.

E. Sample Volume, $D \times \frac{520}{460 + T_m} \times \frac{B.P. + P_m/13.6}{29.9} \times \text{Moisture corr., DSCF}$

F. Concentration, $15.43 \times A/E$, grains/DSCF

G. Stack Gas Flow Rate, DSCFM

H. Emissions, $60 \times G \times F/7000$, lbs/hr

Sampling Station Dalco Outlet Date 2-6-86

WATER VAPOR AND GAS DENSITY CALCULATIONS

Percent Water Vapor in Gases

- A. Gas pressure at meter, In. Hg. (Absolute) 29.74
- B. Vapor pressure of water at impinger temp., In. Hg. .30
- C. Volume of metered gas, Cu. Ft. 32.04
- D. Volume of water vapor metered, B X C/A, Cu. Ft. .32
- E. Volume of water vapor condensed, Cu. Ft. .28
- F. Total volume of water vapor in gas sample, D+E, Cu. Ft. .60
- G. Total volume of gas sample, C+E, Cu. Ft. 32.32
- H. Percent water vapor in sampled gas, 100 X F/G 1.86

Gas Density Correction Factor

Component	Volume Percent/100 x Moisture Correction	Wt./Mole	Mol. Wt. = Wet Basis
Water	.0186	1.0	18.0
Carbon Dioxide	.004 Dry Basis	.9814	44.0
Carbon Monoxide	Dry Basis		28.0
Oxygen	.210 Dry Basis		32.0
Nitrogen & Inerts	.786 Dry Basis		28.2

Average Molecular Weight 28.86

J. Density of gas referred to air = $\frac{\text{Av. Mol. Wt.}}{28.95}$.9967

K. Gas density correction factor = $\sqrt{\frac{1.00}{J}}$ 1.002