



Model Plume Rise

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Current White Paper on Saturated Plumes

- NO_x and SO_x controls can add heat and moisture to stack effluent
- Condensation of moisture in these plumes can increase plume rise
- Plume rise is considered for POINT sources in AERMOD
 - Calculation accounts for both momentum and buoyancy
 - Buoyancy is based on exit temperature and does not consider any additional heat inputs, i.e., the heat of condensation
- PLURIS is generic plume rise model that “can be applied to situations with arbitrary three-dimensional wind fields, arbitrary directions of the source exit, and to both dry and wet plumes”
 - Janicke, U., Janicke, L.: A three-dimensional plume rise model for dry and wet plumes. *Atm. Env.* 35, 2001
- Paine et al., 2016, recommend a pre-processor to adjust POINT source temperature to account for additional buoyancy from condensation
 - Need update to AERMOD formulation that allows for calculation in the model
- Currently no model performance evaluation of the suggested pre-processor



Summary of Buoyant Line Plume

- EPA incorporated the Buoyant Line Plume (BLP) model into AERMOD as part of the 2017 Appendix W update
 - BLP was integrated “as is”, with no scientific changes
 - AERMOD met is converted to PG stability class for BUOYLINE calculations in AERMOD
- BLP was formulated for “roof vents”, mainly for smelter facilities
 - Plume rise from these sources includes buoyancy only, i.e., no momentum
 - BLP considers wind-angle specific entrainment, such that plume rise can be enhanced when winds are parallel to vents
 - BLP has been applied in various ways for other “long and hot” sources

BLP/ BUOYLINE Formulation

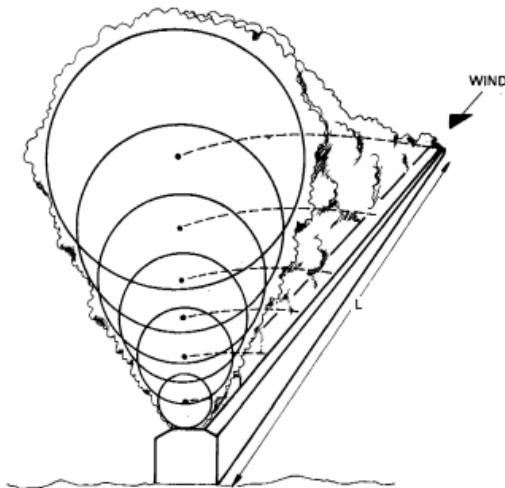
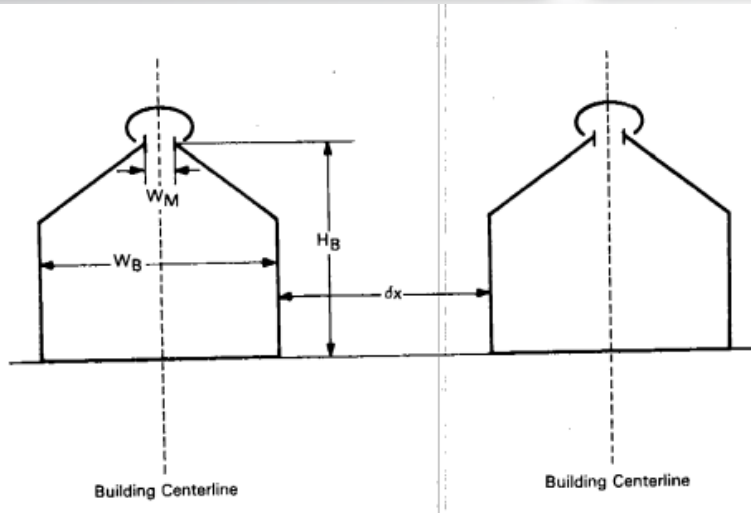


Figure 2-9 Cross Section of Line Source at $X = X_{pg}$ with Parallel Winds

- The buoyance flux for BLP:

$$F' = \frac{g * L * W_m * w * (T_s - T_a)}{T_s}$$

- g is gravity, L is the length of the source, W_m is the width of the source, w is the vertical exit velocity of the vent, T_s is the exit temperature, and T_a is the ambient temperature.

- AERMOD point source buoyance flux

$$F_b = \frac{g * w_s * r_s^2 * (T_s - T_a)}{T_s}$$

- Buoyancy flux formula is essentially the same among the various models



Recent Model Clearinghouse Actions

- Three recent MCH actions, all titled “BLP/AERMOD Hybrid Approach for Buoyant Fugitives in Complex Terrain”
 - 2 coke oven facilities, one in Allegheny, PA and one in Follansbee, WV
 - Both also the subject of MCH records from early 1990’s
 - Hybrid approach seeks to maximize scientific features from both formulations, i.e., enhanced plume rise from BLP, better dispersion estimates from AERMOD POINT/AREA sources



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The challenge of coke ovens

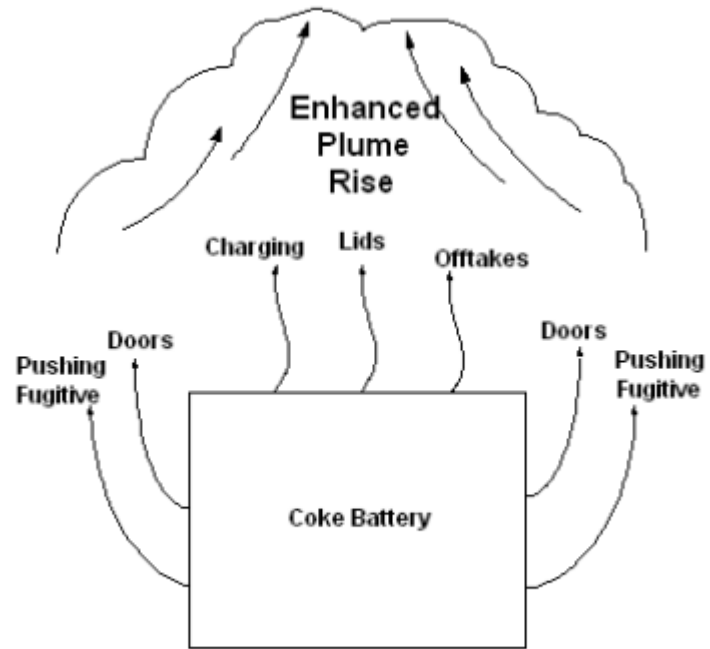
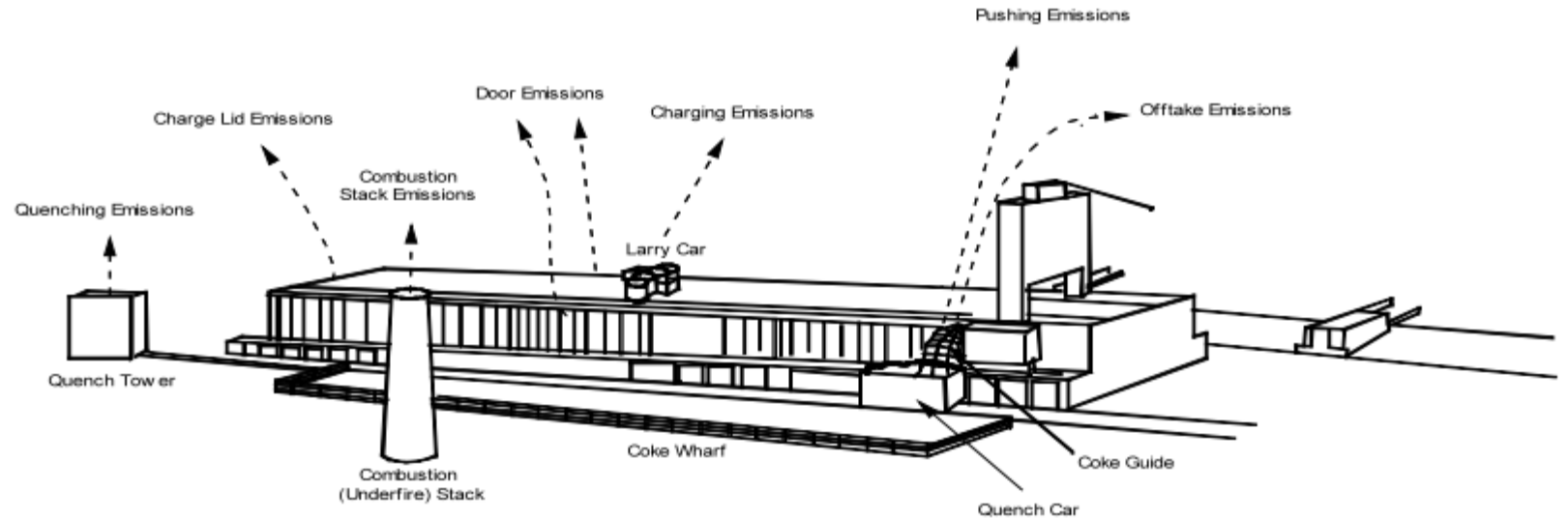


Figure D-1. Enhanced Plume Rise Sources



- - - -> Emission stream



Other features of coke ovens

- Highly variable temperatures
 - Oven surface temperatures 450 F
 - Internal oven temperatures 1800 F
- Highly variable emissions
 - Individual ovens opened and closed constantly along the length of the oven for short periods of time
 - Quench car runs from ovens to quench tower with hot coke
 - Many fugitive emission sources
- Overall buoyancy is not just from emissions
 - RRA computed heat flux from surface heat transfer in addition to flux from emissions



Potential future topics on plume rise

- Buoyancy from fugitives could be important for some sources
- Buoyancy from generally “hot” facilities, even if not the specific emissions themselves, could be important for some sources
- Plume merging from nearby stacks not explicitly accounted for in AERMOD, but another feature of plume rise that could be important
- Plume rise is calculated independently, but plume height important in many other model formulation aspects
 - Interaction with downwash
 - Interaction with top of the mixing layer, i.e., the penetrated plume white paper submitted recently
 - Despite efforts to approach individual model updates, issues are interrelated